Appendix J
Descriptions of Control Equipment

Specification for Baghouse on Lime Cooler Exhaust

Specification for Baghouse On Lime Cooler Exhaust

One F.L.S. Airtech ® Model 210C12(6) Jet-Pulse dust collector designed for the following operating conditions and specifications:

MODEL NO.	210C12(6)
APPLICATION	MATREIAL HANDLING
DUST	LIME
INLET DUST LOAD	40 GRS/ACF
VOLUME	13,280 ACFM 425 F.
DESIGN STATIC PRESSURE	-20 " W.G.
CLOTH AREA	3,959 FT.2
AIR TO CLOTH RATIO	3.35:1

SPECIFICATION FOR F.L.S. AIRTECH, INC. ® MODEL 210C12(6) WALK-IN PLENUM

TYPE JET-PULSE COLLECTOR (ONE COMPARTMENT)

GENERAL

The jet-pulse on line cleaning dust collector is a semi-shop assembled unit with an automatic self-cleaning system that utilizes pulse jets of high pressure air to provide efficient, thorough cleaning with no internal moving parts. Top bag removal, walk-in plenum design, provides the ability to remove the snap-in/out filter bags. Self-supporting cages and venturi nozzles allow for inspection and replacement without tools or clamping mechanisms.

WALK IN PLENUM

One (1) full bag height walk-in clean air plenum, fabricated from 12 ga. carbon steel with sloped roof, welded construction, designed for -20" w.g. internal pressure. Hinged and gasketed access door with quick acting, lever-type latches, one 6" diameter compressed air header, and one blow pipe per row of 15 bags are included.

HOUSING

One (1) compartment bag housing fabricated from 12 ga. carbon steel, welded construction, designed for -20 w.g.internal pressure.

TUBESHEET

Fabricated from 3/16" plate carbon steel with bag support holes spaced on 8" centerlines.

HOPPER

One (1) pyramid type, fabricated from 10 ga. carbon steel, welded construction, designed for -20" w.g. pressure and 65 lbs./ft.³ bulk density at 2/3 hopper height. The hopper slide slope is 60 minimum side slope with 53 minimum valley angle. Access door is fabricated steel hinged and gasketed.

SERVICE PLATFORM

One external platform at tubesheet level, complete with 1" \times 3/16" bar grating, 4" \times 1/4" toeboard, 1" diameter handrails, and 2-1/2" \times 3/8" handrail post.

STRUCTURAL SUPPORTS

Supports provide 4'-0" clearance under the discharge of the rotary lock. Columns and bracing are designed to withstand 30 lbs/ft.2 and 100 mph windload.

LADDER/CAGE

One safety caged ladder to provide access to the tube sheet platform.

PAINT

External single coat of shop primer on SSPC-SP2 (hand tool cleaning).

BAGS

One (1) compartment bag housing fabricated from 12 ga. carbon steel, welded construction, designed for -20 w.g.internal pressure.

TUBESHEET

Fabricated from 3/16" plate carbon steel with bag support holes spaced on 8" centerlines.

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LADDER/CAGE

One safety caged ladder to provide access to the tube sheet platform.

PAINT

External single coat of shop primer on SSPC-SP2 (hand tool cleaning).

BAGS

Made from 6" diameter x 12'-0" long 16 oz./yd² woven fiberglass with snap-in bag collar. Maximum operating temperature is 500 F.

The dust collector contains 14 rows of 15 bags per row, for a total of 210 filter bags representing 3,956 ft.² cloth area.

CAGES

Fabricated in one piece, made of twenty vertical 11 ga. carbon steel wires, solid bottom cap, and protective bag collar.

VENTUR!

The venturi is manufactured by a metal spinning operation made from 18 ga. carbon steel. It is flange supported and fastened to the cage top collar.

PULSE VALVES

One pulse valve for each row of bags, mounted on air header. Solenoid valves are grouped in enclosures.

PRESSURE GAUGE

One magnehelic pressure gauge to register pressure differential across the dust collector. The gauge is furnished with 20'-0" of tubing, and fittings for field mounting.

TIMER

Automatic sequential controllers that activates the solenoids, which controls the pulse valve for each bag row. Controls are provided to adjust the length of time between valves being energized and the length of time that the valve is energized. Solid state timer, Model WJ in NEMA 4 enclosure for 115 V, single phase, 60 Hz.

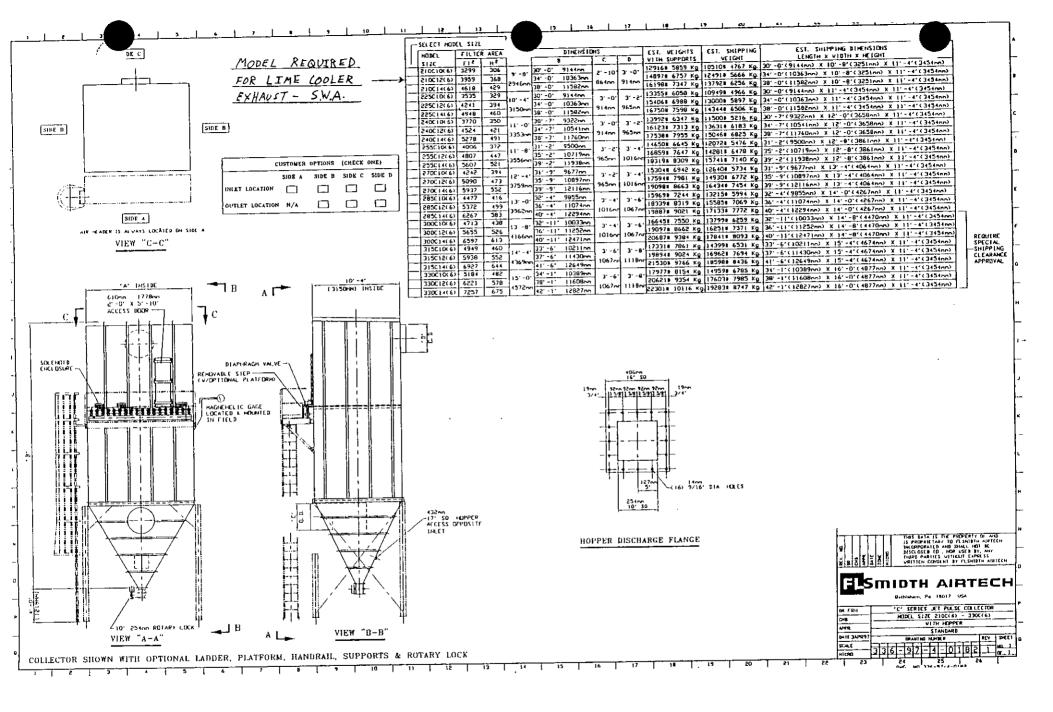
DUST DISCHARGE SYSTEM

One (1) rotary lock with 1/2 H.P. T.E.F.C. motor, for pyramid hopper discharge.

ASSEMBLY

The dust collector is shipped in pre assembled sections for field assembly. Bags, cages with venturis, valves, timer, rotary lock, and any equipment offered as an add-on item, are shipped separately for field installation.

cdm210c



Specification for Dry Electrostatic Precipitator

Specification for Dry Electrostatic Precipitator

SPECIFICATION

FOR

DRY ELECTROSTATIC PRECIPITATOR

County of Palm Beach, Florida Lime Reburning Kiln

Prepared by Camp Dresser & McKee

SPECIFICATION NO.

REV	DATE	DESCRIPTION	PAGES	BY	APPROVED BY
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TABLE OF CONTENTS

1.	SCOPE		1
	1.1 Application	n	1
	1.2 Equipmen	t and Services by Bidder	1
	1.3 Equipmen	t and Services by Others	4
	1.4 Terminal I	Points	4
	1.5 Information	on Required	5
	1.6 Performar	nce Guarantee (To be part of Contract)	8
2.	DESIGN DATA		10
	2.1 General		10
	2.2 Lime Kiln	Precipitator	10
	2.3 Structural	Design	11
	2.4 Miscellan	eous Criteria and Services	11
3.	DETAILED REQU	JIREMENTS OF EQUIPMENT	12
	3.1 Standards	s and Codes Applicable	12
	3.2 Precipitat	or	13
	3.3 Precipitat	or Ash Collection System	13
	3.4 Precipitat	or Discharge Electrodes	13
	3.5 Precipitat	or Collecting Electrodes	14
	3.6 Precipitat	or Electrode Rapping System	14
٠.	3.7 Structura	l System	14
	3.8 Electrical	Requirements	15
		and Lagging	17
	3.10 Accessor	ies	. 18
5.	QUALITY PROV	ISIONS	19
	5.1 Construc	tion/Erection Advisor	19

PAGE NO.

1. SCOPE

1.1 Application

This specification is for an electrostatic precipitator and accompanies for County of Palm Beach Florida, Camp Dresser & McKee Company Project No.xxx.

The Bidder shall design, furnish, fabricate, and deliver one (1) electrostatic precipitator complete with all components, accessories, and services mandated by this specification. It is not the intent of this document to specify completely all of the details for design and construction of this equipment. However, the equipment shall conform in all respects to high standards of engineering, design, and workmanship.

The precipitator shall be designed for particulate removal on a lime reburning kiln. The precipitator shall be of a single chamber design. The precipitator shall be shop fabricated to the greatest extent practical.

The precipitator bid shall be confined to an arrangement and design which has been proven by past operating experience in existing units of comparable capacity and design conditions. A list of such installations where precipitators of similar design are in service shall be provided with the quotation.

1.2 Equipment and Services by Bidder

The intent of this section is to outline the major portions of the Bidder's scope of supply. This listing is not all-inclusive and the Bidder shall provide complete operable systems.

1.2.1 Structural

	Bidder	<u>Others</u>
 a. Precipitator support steel design and supply 	X	
b. Foundations design and supply		Χ
c. Anchor bolts		X
 d. Design and supply of ductwork from induced draft fan to precipitator inlet plenum 		X
 Review design of ductwork from induced draft fan to precipitator inlet plenum 		X

		<u>Bidder</u>	<u>Others</u>
	f. Access facilities (stairs, ladders, walkways, platforms, and handrails) from grade and boiler building to top of precipitator	X	
	g. T-R monorail system including hoists and motors	×	
	h. Shop painting	X	
	i. Touch-up painting		x
	j. Insulation	Engineer -ing only	X
1.2.2	Mechanical		
		<u>Bidder</u>	Others
	a. Penthouse blower system	X	
	b. Inlet and outlet plenums	Х	
	c. Inlet and outlet expansion joints		X
	 d. Inlet and outlet gas distribution devices 	x	
	e. Access doors	X	
	 f. Precipitator bottom hoppers and outlet rotary valves 	×	
	g. Ash collection, transport, and storage system		x
	h. Collecting electrodes	X	
	i. Discharge electrodes	x	
	j. Rapper system	×	
	k. I.D. fan		X
	I. Stack		X
1.2.3	Electrical/Controls		
		<u>Bidder</u>	<u>Others</u>
	a. Transformer rectifiers	X	

. . . .

		<u>Bidder</u>	Others
b.	Bus bar and bus ducts	×	
c.	Rectifier control consoles	×	
d.	Undervoltage relay protection	×	
e.	Rapper controls and panels	x	
f.	Alarm point outputs to DCS	×	
g.	Grounding of precipitator		X
h.	Safety key interlock system	×	
i.	MCC/electrical distribution panel		x
j.	Field mounted instruments		х
k.	Interface connections for remote operations	x	
1. 1	Motors integral to equipment fumished	x	
m.	Low voltage electrical power wiring, control wiring, and lighting		X
n.	Non-integral standard NEMA frame motors, starters, and contactors, unless specifically included in this specification		. X
О.	 Motor control center for precipitator to include: 1. Combination starters for the rappers, if required 2. Combination starters for the fans, etc., as required 3. 110 V controls as applicable. 		×
p.	Hardware/software required for DCS interface	×	
q.	Penthouse pressure & temperature transmitters.	X	
r.	Flue-gas pressure & temperature transmitters each field & outlet plenum		x

		<u>Bidder</u>	<u>Others</u>
a.	304 Stainless steel name tags on all equipment and instruments.	X	
b.	Engineering design specification for insulation and lagging and attachment.	X	
c.	Erection of precipitator		×
d.	Construction/Erection/QA advisor(s)	x	
e.	Start-up engineer(s)	×	
f.	Performance test		X
g.	Training program for plant personnel (see option)		X
h.	Operations and maintenance manuals	x	
i.	Priced spare parts list	x	
j.	Spare gasket for each door	x	
k.	Air conditioned control/electrical room		X

1.3 Equipment and Services by Others

See Paragraph 1.2.

1.4 Terminal Points

The terminal points list is included to clearly identify end points of equipment supplied. All equipment on the precipitator side of each point shall be supplied.

1.4.1 Flue Gas

- a. Inlet flange of precipitator inlet plenum.
- b. Outlet flange of precipitator outlet plenum.

1.4.2 Ash

Outlet flange of precipitator hopper rotary valves.

1.4.3 Electrical

Equipment up to and including T/R distribution cabinet, T/R console and rapper control cabinet.

1.4.4 Structural

Owner furnished support steel and foundations.

1.4.5 Ambient Air

Inlet to silencer (id required) for penthouse blower(s).

1.5 Information Required

1.5.1 Information Required with Proposal

a. Outline drawings showing general arrangement, approximate weights, dimensions, sampling and instrument port locations, and space clearance requirements for proposed equipment including platforms, ladders, column locations, and loads.

The Bidder shall provide copies of general drawings in AutoCAD 2000 on 3 1/2-in. computer disk or CD.

- **b.** Specifications and descriptive data on proposed equipment, including detailed equipment and motor list, showing: horsepower, rpm, and application data.
- c. Completed Bidder Data Sheets, Attachments A and B with all blanks filled in. For consideration, the Bidder must complete the attached data sheets. The requested information in any other format is not acceptable for evaluation.
- d. Submit correction factors in the form of performance guarantee curves. Performance test data will be corrected for actual operating conditions from these curves in the determination of conformance with performance guarantees. Correction factors for capacity shall as a minimum range from 70 percent to 110 percent of design gas flow. The Bidder shall identify the design operating point on each curve.

Submit the following curves for the precipitator and state the accepted method for interpolation of the curves:

(1) Guaranteed particulate emission values plotted against varying gas flow (acfm) for a range of inlet dust loadings. As a minimum, the range of inlet dust loadings shall include 50 percent to 200 percent of the design inlet loading.

- (2) Guaranteed draft loss values (inches wg) plotted against varying gas flow (acfm).
- e. Names and addresses of installations, within the last 10 years, of similar design and same equipment.
- f. ANY EXCEPTIONS TO THIS SPECIFICATION MUST BE LISTED CLEARLY IN THE PROPOSAL. Should there be serious objections which would prohibit giving a competitive bid, the Engineer shall be notified, in writing, so that changes can be considered and all Bidders notified. If in full compliance with this specification, so state in proposal. This specification shall serve as the Owner's technical portion of the purchase order.
- **g.** Statement of performance guarantee based upon precipitator design criteria and fuel data given in Section 2.0.
- h. Furnish tabulations, lists, write-ups, or other suitable descriptions defining the extent to which furnished equipment and materials are factory assembled.
- i. Bidder's drawing schedule showing dates of submittal of all Bidder drawings to include both initial and final submittal (See data needs list, Attachment C). Attachment C must be completely filled in, expanded, as required, and returned with bid. The Owner and Engineer shall review all preliminary drawings and return them to the Bidder's facility within fifteen (15) working days from receipt of same. All dates shall be from award of verbal purchase order.
- j. The Bidder shall submit a copy of Bidder's Quality Assurance/Quality Control Program.
- **k.** Master Bill of Materials list sample.

See Section 1.5.2.c.

1.5.2 Information Required with Contract

- a. Approval Drawings to the Owner and Engineer shall include, but not necessarily be limited to, the following:
 - (1) Precipitator arrangement drawings include front, rear, both sides, and top views in sufficient detail to allow setting of interconnecting platforms and to identify all access points and clearances required for equipment

- removal. Show Owner interface points, loads, and breeching movements.
- (2) Foundation load requirements to include dead load, live load, wind, thermal and/or seismic loads at each load point. Drawing should show all loads and load points. Load diagrams identifying fixed and expansion load points with expansion load point movements.
- (3) Electrical system single-line diagrams to show all Bidder furnished items as well as items to be furnished by Owner.
- (4) Terminal plans and connections for all electrical and process control/indication/monitoring equipment and control panels shall show all Owner connection points both schematically and physically.
- (5) Elementary wiring diagrams for the control of all motor operated devices and magnetic contactors supplying other electrical loads.
- (6) Instrumentation loop sheets, specification sheets, and installation details for all instrument devices used for process control, monitor, or indication purposes.
- (7) Panel outline drawings showing physical dimensions of all Vendor furnished panels.
- b. Operating and Maintenance Instruction Manuals, 12 required, in accordance with the attached INSTRUCTIONS TO BIDDERS, shall be provided to the Owner by the Vendor and shall contain at least the following:
 - (1) Description and assembly drawings of each item of furnished equipment.
 - (2) Parts nomenclature.
 - (3) Wiring and piping diagrams.
 - (4) Procedures for start-up, troubleshooting, and operation of unit.
 - (5) Instructions for assembly and reassembly of all items of equipment furnished as required for normal operation and maintenance.

- (6) General arrangement drawings.
- (7) Precipitator guarantee and performance data including performance and emissions curves.
- c. The Vendor shall provide a Master Bill of Materials list to the Owner and Engineer. This list shall be received no later than 2 months prior to the start of precipitator delivery.

The list is to be suitable for use as a check list to verify field receipt of all Vendor's fabrications, piece parts, sub-supplier equipment and materials to be furnished, delivered, as a part of the purchase order.

The Bidder shall include a sample master bill of materials list in the proposal.

1.6 Performance Guarantee

1.6.1 Acceptance Test

- a. An Acceptance Test to evaluate operating performance against the performance guarantees shall be performed for the precipitator by the Owner or his designee. The tests will be conducted at a mutually agreed time within the warranty period as set forth in the Purchase Agreement. The Vendor shall witness all acceptance tests.
- b. Prior to conducting an Acceptance Test, the precipitator shall be operated through a minimum two (2) week period without equipment or operations modifications except for routine maintenance.
- c. For all performance guarantees, three (3) test runs performed by the Owner shall establish an acceptance test value. Performance guarantee curves (as described in paragraph 1.5.1 e) shall be used to evaluate test data for actual operating conditions. The average of the three- (3) test runs must achieve the performance guarantee to demonstrate particulate emissions compliance.
- **d.** The precipitator must demonstrate compliance with the performance guarantee in order to be accepted by the Owner as having passed its respective acceptance test.
- e. The Owner shall notify the Vendor of whether a precipitator passes or fails its respective acceptance test.

- f. In the event that a precipitator fails to demonstrate performance equal to or superior to the performance guarantees, the Vendor shall have a period of 60 calendar days for equipment or operation adjustments and re-testing. This 60-day period begins with the Owner's notification to Vendor of a precipitator's acceptance test failure.
- g. If a precipitator fails to demonstrate compliance with its performance guarantees within the 60-day period for adjustments and re-testing, then the precipitator shall be deemed in non-compliance with the specification. In this event, the rights and responsibilities of the Vendor and Owner shall be as set forth in the Purchase Order.
- h. The entire cost, including freight and labor, for any additional testing or equipment modifications in order to satisfy a performance guarantee shall be borne by the Vendor. Any work or required downtime for these purposes shall be at the Owner's convenience.

i. Particulate Emission Tests

The particulate removal efficiency and emissions of the precipitator shall be determined by measuring the particulate content of the incoming and effluent gases. These measurements shall be taken at the inlet and outlet plenum ducts in accordance with EPA Test Method 17, EPA Standards of Performance for New Stationary Sources (40 CFR Part 60).

Condensables will not be included in the determination of particulate collection efficiency.

j. Draft Loss

The draft loss across the precipitator shall be measured by performing traverses of the inlet and outlet plenum ducts. The traverses shall be performed in accordance with EPA Method 1. The measured draft losses shall be corrected for actual operating gas flows using the guaranteed correction curve (as described in paragraph 1.5.1.e.2).

1.6.2 Performance

Performance guarantees shall be provided with the proposal, stating that the electrostatic precipitator system will meet the range of operating requirements listed in Section 2.0.

The Bidder's proposal shall include the following performance quarantees for the precipitator.

- a. The Bidder shall guarantee a maximum draft loss at design gas flow conditions for the precipitator. The draft losses shall be measured from the precipitator inlet plenum to the precipitator outlet plenum.
- **b.** The precipitator particulate emission shall not exceed the limits given in the following table:

	Guaranteed Performance
Lime Reburning Kiln Precipitator Grains/DSCF, 3 hour test average	0.010

(1) All emissions data shall be based on EPA measurement standards.

2. DESIGN DATA

2.1 General

The precipitator shall be designed for continuous, heavy-duty, 24 hour per day, service. Only materials and workmanship suitable for this service and which will require minimum maintenance and downtime shall be used. The precipitator shall be remotely operated and monitored from an operator control room located approximately 500 feet away.

2.2 Lime Reburning Kiln Precipitator

- 2.2.1 Installation will be downstream of a lime reburning kiln with an induced draft fan.
- 2.2.2 The precipitator shall be designed for the specified gas flow while satisfying the criteria for maximum allowable particulate emissions (paragraph 2.2.4. f).

- 2.2.3 In no case shall the emissions level be greater than the maximum values given in 2.2.4. The Bidder shall take all necessary corrective actions to achieve these guarantees.
- 2.2.4 The combination fuel power boiler electrostatic precipitator design criteria is as follows:

a. Flue Gas Flow, ACFM	Design	24,876
b. Gas Density, lb/ft ³	Design	0.0363
c. Flue Gas Temp., °F	Design Operating	550
	Structural Design	650
d. Flue Gas Moisture, % vol.	D 00.ig.1	33.72%
e. Inlet grain loading, gr/acf		20.0
 f. Outlet particulate load, gr/DSCF-design 		0.010

2.3 Structural Design

2.3.1 The following design criteria shall be the basis for all structural design of the precipitators and related equipment:

a. Metal temperature, °F 650

b. Internal pressure, in. water - 10

2.4 Miscellaneous Criteria and Services

- 2.4.1 The precipitator shall be installed and operated at elevation 10 feet nominal above mean sea level. All drawings shall reference grade elevation as "actual."
- 2.4.2 The precipitators shall be installed outdoors. The ambient temperature range is 10°F to 100°F.
- 2.4.3 The equipment shall be designed and supported to withstand seismic and wind forces in accordance Note need FL codes

2.4.4 The following utility services will be available. All remaining utility services to the precipitator shall be provided by the Bidder.

a. Compressed air

60 psig

b. Instrument air

60 psig,

-10°F wet bulb

c. Water

50 psig, 98°F at grade

d. Electrical

120/240 Volt, 1-phase, 60-hertz; 480 Volt, 3-phase, 60-hertz; 4160

Volt, 3-phase, 60-hertz

3. DETAILED REQUIREMENTS OF EQUIPMENT

3.1 Standards and Codes Applicable

3.1.1 All applicable codes in effect as of the date of purchase and any subsections thereof, as applicable, shall govern design, fabrication, testing and selection of equipment and materials supplied. These include, but are not limited to, the following:

AISC	American Institute of Steel Construction		
AISI	American Iron and Steel Institute		
ANSI	American National Standard Institute		
ASCE	American Society of Civil Engineers-Minimum		
	Design		
ASCE7	American Society of Civil Engineers-Minimum		
	Design Loads for Buildings and Other Structures		
ASME	American Society of Mechanical Engineers		
ASTM	American Society of Testing Materials		
AWS	American Welding Society		
EPA	Environmental Protection Agency		
IEEE	Institute of Electrical and Electronic Engineers		
IGCI	Industrial Gas Cleaning Institute, Inc.		
NEC	National Electrical Code		
NEMA	National Electrical Manufacturers Association		
NFPA	National Fire Protection Association		
OSHA	Occupational Safety and Health Act		
FBC	FLORIDA Building Code		

3.1.2 Local, state, and federal regulations in effect as of the date of purchase shall be complied with.

3.1.3 Bidder shall warrant that all materials, equipment, and other items furnished by Bidder in connection with this specification and that Purchaser's use in accordance with Vendor's operating instructions shall comply with all such applicable laws, rules, regulations and codes.

3.2 Precipitator

- **3.2.1** Bidder shall quote maximized shop assembly of the unit and provide an estimate of field erection time and labor.
- 3.2.2 The precipitator shall be of single chamber design. The chamber walls and roof shall be of single wall construction with external stiffeners as required.
- 3.2.3 All seams and joints inside the precipitator shall be seal welded.
- 3.2.4 Provide a ventilated weatherproof roof enclosure complete with structural steel framework, and ribbed aluminum roofing, to cover the transformer/rectifiers and other penthouse roof mounted equipment.
- 3.2.5 Monorail beams shall be provided for transporting and lowering precipitator equipment to the ground level from penthouse roof.
- 3.2.6 The penthouse of the precipitator shall be gas-tight and provided with a positive pressure ventilation system supplied with heated, clean air to prevent condensation. The necessary temperature switches and control devices for the heater/blower set operation shall be included.

3.3 Precipitator Ash Collection System

- 3.3.1 Bidders shall furnish a rotary valve on the outlet of each ash hopper.
- 3.3.2 The ash collection system downstream of hopper outlet rotary valves shall be by Owner.
- 3.3.3 Precipitator hopper electric heaters with maintenance access shall be furnished as recommended.

3.4 Precipitator Discharge Electrodes

3.4.1 The discharge electrode system preferred shall be either of the rigid frame or rigid electrode design.

3.4.2 A steel or alloy steel suitable for the service specified shall be the material of construction.

3.5 Precipitator Collecting Electrodes

- 3.5.1 The collecting electrodes shall be constructed of steel or alloy steel suitable for the service specified.
- 3.5.2 Height of collecting electrodes shall be selected to minimize reentrainment of ash during rapping.

3.6 Precipitator Electrode Rapping System

- 3.6.1 A complete mechanical rapping system shall be provided. The rapping system shall be of the mechanical type with "tumbling hammers" installed on a rotating shaft. To minimize rapping spikes, one rapper will be required for each collector sheet.
- The rappers shall operate in a manner such that maximum dust collection will be maintained during the rapping process.
- 3.6.3 All rapper controls and drive mechanisms shall be located such that they are accessible for maintenance without shutting down the precipitator. All necessary passages through the precipitator enclosure shall be sealed watertight.
- 3.6.4 Each electrical field shall be separately rapped in order to reduce the percentage of the treatment zone that can be disturbed at any time.
- 3.6.5 The Bidder shall provide a list of all monitoring and control variables (such as status, start/stops, alarms, etc.) for interface to a distributed control system.

3.7 Structural System

3.7.1 Supporting Structure

- plenum, chamber, and outlet plenum including all columns, girders, and beams down to the expansion bearing plate interface plane. Precipitator structure shall accommodate loads for walkways.
- b. Supply these loads itemized as follows:

Loads at each column point:

Dead Load
Live Load
Wind Shear-N/S Axis
Wind Shear-E/W Axis
Wind Axial Load-Uplift
Wind Axial Load-Compression
Seismic Shear-N/S Axis
Seismic Shear-E/W Axis
Seismic Axial Load - Uplift
Seismic Axial Load - Compression

3.8 Electrical Requirements

3.8.1 General

All insulators and wiring materials required to electrically connect the transformer/rectifier units to the precipitator electrodes shall be provided. The high voltage lead from the rectifier to the precipitator shall consist of a conductor in a bolted metal-enclosed weatherproof bus duct, allowing for disassembly. Electric space heaters shall be provided for operation on 120-volt, 60-Hz source. The bus duct shall include necessary insulators and duct supports and fittings, and shall be supplied, formed to exact length, ready for bolting to the equipment.

3.8.2 Transformer/Rectifier Units

- a. The transformer/rectifiers shall be located on top of the cold roof and preferably be of the same size. The access doors to all electrically hazardous areas shall be key interlocked (Kirk preferred) with the main supplies and adequate grounding provisions made for personnel safety. This equipment shall be designed such that the plant area shall be free from any radio noise or interference caused by the rectifiers when operating. Supply a key for each door. Only one set of keys shall be furnished. All keys/locks shall be accessible without hazards to personnel.
- b. Each high voltage transformer shall be a single phase, silicon oil immersed, self-cooled unit contained in a welded steel case. Transformers shall have copper windings, i.e., aluminum not acceptable. Transformers shall be rated for 55 °C rise OA at base kVA rating.
- c. The rectifier shall be full-wave type. Each rectifier set shall be mounted directly on its respective high voltage transformer case.

- d. Each transformer/rectifier shall be mounted on a base which forms a tank or containment vessel of sufficient volume to contain the entire quantity of oil in the transformer in order to prevent loss of this fluid to the surrounding area in the event of leakage.
- e. The primary voltage supply to the transformer will be 480-volt, single-phase, 60-hertz.
- f. High voltage insulators shall be 85 percent fused alumina and shall be located out of the gas stream.
- g. Each transformer/rectifier shall be provided with a temperature gauge, liquid level gauge, sampling connections, drain valve, and weatherproof terminal box with gasketed removable cover. The terminal box shall contain transformer primary connections, rectifier positive terminals, ground terminal, and interface to control electronics.
- h. The high voltage connections from the T/R unit to the electrode bus sections shall be enclosed in a weatherproof, corrosion-resistant bus duct. The high voltage connection to each bus section shall have a disconnect switch that when opened will ground the electrode. The disconnect switchblades shall be visible for verification of switch position. Access to the high voltage disconnect switch shall be secured by a key interlock switch. This switch shall be keyed to the open position of the disconnect switch in the TR set primary winding.
- i. The Vendor shall provide a list of all monitoring and control variables (such as status, start/stop, alarms, etc.) for interface to a distributed control system.
- j. Interior of bus duct and air switches shall be covered with a white epoxy coating.

3.8.3 Transformer/Rectifier Control Cabinet

- a. Provide a NEMA 12 transformer/rectifier (T/R) control cabinet to be housed in the motor control center room.
- **b.** The T/R control cabinet shall house a main circuit breaker, key-interlocked to the precipitator access doors, and the T/R transformer controls.

- c. The T/R control cabinet shall house all contactors, control transformers, branch circuit protection, rectifier protection devices, indicating instruments (including a-c and d-c ammeter and, a-c and d-c voltmeter), timers, overcurrent protection systems and rectifier's undervoltage power and control system, plus local control devices on door and provisions for remote alarm.
- d. Provide a 480/120 volt transformer and panelboard for supplying all 120-volt a-c necessary for the control of the rectifier units. This equipment shall also be housed in the T/R control cabinet.

3.8.4 Rapper Controls

Rapper controls shall be integral with the Automatic Voltage Controllers.

3.8.5 Alarms

Contacts shall be furnished for the alarms to be located in the mill control room. The annunciation will be part of the distributive control system, and the required interface devices shall be provided. The Bidder's proposal shall include a list of alarms.

3.8.6 Grounding

Devices for positively grounding the high-voltage system of the precipitator prior to personnel entering the enclosure shall be provided. The bus duct disconnect switch shall ground the precipitator when opened.

3.9 Insulation and Lagging

- 3.9.1 Supply engineering design specification for insulation and lagging for all exposed surfaces of the precipitator and related equipment. Insulating materials shall be securely anchored to the insulated surface. Lagging shall not serve to support or hold insulation in place. All insulation material shall be non-asbestos.
- 3.9.2 Where required for inspection and maintenance purposes, insulation and lagging shall be installed in readily removable and replaceable sections, i.e., hinged doors with latches. Where near-horizontal areas may be exposed to occasional foot traffic, lagged

insulation shall be adequately stiff to support such traffic without distortion of the insulation or lagging.

3.9.3 Specify type and thickness of insulation and lagging. Insulation shall be of sufficient thickness (4-in. minimum) to ensure a surface temperature not to exceed 130°F with a ambient temperature of 100°F and an air velocity of 50 feet per minute at the face of the lagging. Insulation will also maintain the inside surface of the precipitator above the dew point with ambient air temperature as specified herein and a wind velocity of 50 feet per minute at the face of the lagging.

3.10 Accessories

3.10.1 Access Doors

a. Access doors shall be of the dust-tight, hinged design with internal insulation and compression latch mechanism. The exterior shall be hot-dip galvanized.

b. Access doors shall be furnished as follows:

- (1) In the precipitator shell—not less than one door between each adjacent pair of electrical fields located at the elevation of the bottom of the electrodes.
- (2) In precipitator roof (hot roof deck)—one for access to each bus section.
- (3) Inlet and outlet plenum where applicable—one in each plenum.
- (4) Other—Furnish other doors as required wherever his design dictates to ensure proper operation, inspection, cleaning, and maintenance of the equipment.

3.10.2 Key Interlocks

All access doors through which personnel might come in contact with high voltage equipment shall be key-interlocked to prevent opening before the precipitator power supply is de-energized and the equipment connected to ground. All locks and keys shall be constructed entirely of Type 304 or Type 316 stainless steel, and the exposed portions shall be housed in a steel enclosure with a hinged and gasketed cover.

3.10.3 Ductwork and Breeching

- **a.** The precipitator inlet and outlet plenums shall be provided by Bidder, and designed to be self-supporting.
- b. Duct layout to precipitator inlet plenum and from the precipitator outlet plenum will be submitted to the Precipitator Vendor for review. It shall be the responsibility of the Precipitator Vendor to assure the duct layout and design will give an even gas distribution within the precipitator. It shall be the responsibility of the Precipitator Vendor to mark on these drawings all of the necessary test connections and nozzles for testing of the unit upon completion of erection.

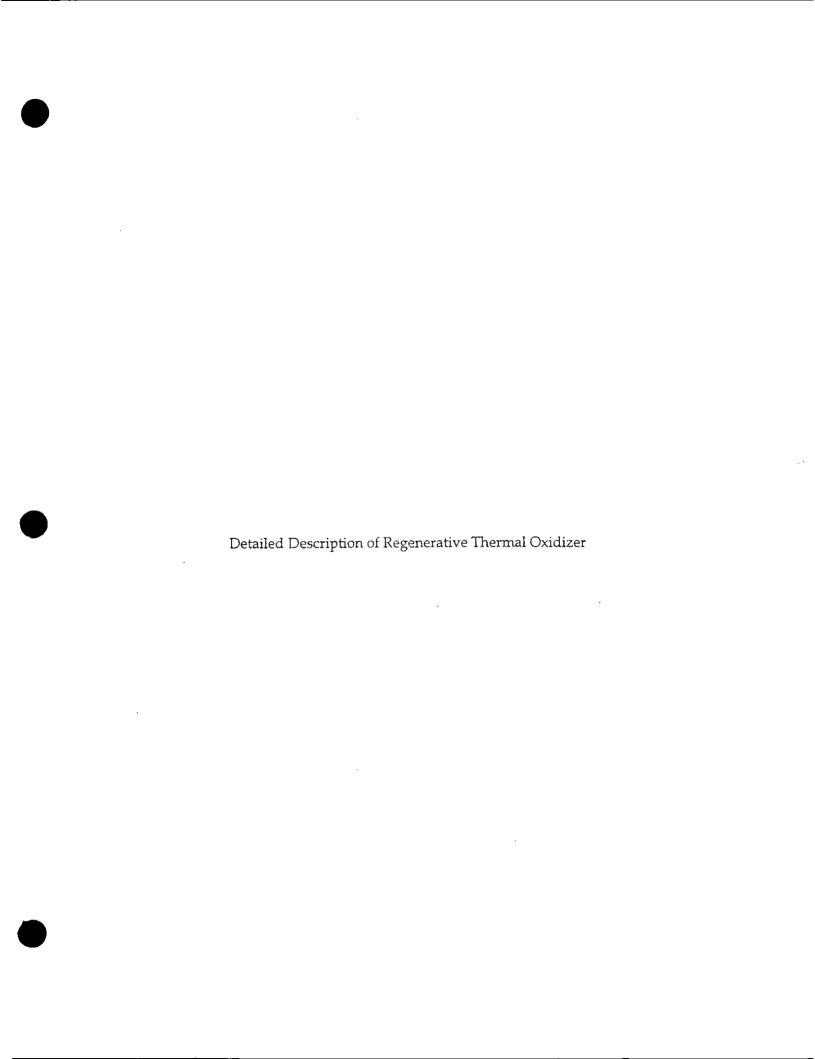
3.10.4 Controls

- a. Supply a recommended control diagram for equipment reflecting the necessary minimum controls and interlocks required for precipitator operation. Quote all solid state controls.
- **b.** All pertinent alarms and status indications shall be wired to the mill's digital control system as 4-20 mA signals.
- **c.** Furnish as an option, provisions for a digital interface for all control signals to the Owner's DCS.

4. QUALITY PROVISIONS

4.1 Construction/Erection Advisor

- 4.1.1 The Bidder shall include with materials supply, the services of a Construction/Erection Advisor, full time during installation of the precipitator.
- 4.1.2 The Vendor's Construction/Erection Advisor shall have full authority to act on the Vendor's behalf in order to monitor construction quality control, provide weekly progress reports to the Owner, and advise Owner of potential construction discrepancies, omissions, or deviations from approved drawings and specifications.
- 4.1.3 The Construction/Erection Advisor shall be available on the jobsite until completion of the installation of all Vendor supplied materials. This shall include any subcontract supply items.
- 4.1.4 Release of the Construction/Erection Advisor by Owner shall be effective upon conditional acceptance of all Vendor supplied equipment for initial operation.



Detailed Description of Regenerative Thermal Oxidizer

A Detailed Description of a Particular Manufacturer's Regenerative Thermal Oxidizer is presented in Appendix M in the O&M Manual of the CECO Abatement Systems Regenerative Thermal Oxidizer System

SECTION 13267

REGENERATIVE THERMAL OXIDIZER

PART 1 GENERAL

1.01 SCOPE OF WORK

- A. Furnish all labor, materials, equipment and incidentals necessary and install complete and performance test regenerative thermal oxidizing equipment as shown on the Drawings and as specified herein.
- B. The following equipment is included under this Section:
 - 1. One regenerative thermal oxidizer.
 - 2. Electrical devices and controls.

1.02 RELATED WORK

- A. Electric motors are included in Section 01171.
- B. Field painting is included in Section 09902.
- C. Refer to Section 11000 for additional specific technical requirements.
- D. Induced draft fans are included in Section 15861.

1.03 SUBMITTALS

- A. Submit, in accordance with Section 01300, shop drawings showing details of fabrication, electrical control diagrams, anchor bolt drawings, erection and adjoining equipment interfaces for all equipment furnished under this Section.
- B. Submit complete wiring diagrams, cabinet and device layout drawings.
- C. Provide samples of ceramic bed material and all types of insulating materials required.
- D. Provide guarantee for regenerative thermal oxidizer thermal efficiency and hydrocarbon destruction.
- E. All design calculations and shop drawings shall be prepared by or under the supervision of a professional engineer registered in the State of Florida, who shall stamp these calculations and drawings.
- F. The supplier shall furnish design calculations to the Engineer for review for conformance with applicable criteria. Calculations shall be in proper sequence, clear and complete. The review of these calculations shall not relieve the supplier of any obligation or responsibility contained in the contract.

JOB NO./1096 13267-1

G. The RTO supplier shall furnish as part of the shop drawing review process a detailed written warranty from the equipment manufacturer stating that this equipment package will perform as stated in PART 1, and, further that, in the event that the equipment does not perform as required, supplier will make such modifications as are necessary to achieve compliance or replace the equipment as required all at no additional cost to the Owner. In the event that the equipment meets the mechanical and process requirements but exceeds the thermal efficiency limits, the manufacturer shall warrant that it will pay damages equal to the difference between actual and warranty consumption based on the then current energy rate and 87,600 hours (10 years) for each unit so deficient.

H. Operation and Maintenance Data

- 1. Provide, in accordance with Section 01730, copies of operation and maintenance manuals and equipment start-up reports.
- 2. Services of a manufacturer's representative shall be provided in accordance with Section 13265.

1.04 REFERENCE STANDARDS

- A. American Society for Testing and Materials (ASTM)
 - 1. ASTM A36 Standard Specification for Carbon Structural Steel.
 - 2. ASTM A240 Standard Specification for Heat-Resisting Chromium and Chromium-Nickel Stainless Steel Plate, Sheet and Strip for Pressure Vessels.
- B. American Welding Society (AWS)
 - 1. AWS D1.1 American Welding Society Code.
- C. Factory Mutual (FM)
- D. Underwriters Laboratories (UL)
- E. National Electrical Manufacturers Association (NEMA)
- F. Where reference is made to one of the above standards, the revision in effect at the time of bid opening shall apply.

1.05 QUALITY ASSURANCE

A. The equipment specified under this Section shall be furnished by a manufacturer who is fully experienced, reputable and qualified in the manufacture and assembly of the equipment furnished. Upon request, furnish to the Engineer the manufacturer's qualification data including value of like work, location and references.

B. Coordinate the interface between the RTO and associated equipment. All necessary engineering drawings and details shall be furnished to the Engineer.

1.06 SYSTEM DESCRIPTION

- The regenerative thermal oxidizer (RTO) shall be a ceramic bed type which shall oxidize odorcausing constituents in the gas stream to non-odorous products of combustion. The RTO shall be designed for a minimum of 92 percent thermal efficiency as defined by Thermal Efficiency = Combustion Chamber Temp - Out Temp/Combustion Chamber Temp - In Temp. The RTO shall have a minimum incineration temperature of 1450 degrees F and shall be designed to operate continuously at 1800 degrees F. The incineration temperature is the average temperature of the combustion chamber of the RTO which shall be maintained as a continuous operating condition. The RTO shall be designed so that the combustion chamber shall have a gas residence time of at least one second at its design incineration temperature and shall be designed for a destruction efficiency of not less than 95 percent of the hydrocarbon inlet loading or a discharge limit of 50 ppm as methane, whichever is less stringent. The RTO shall consist of a combustion chamber which feeds three energy recovery chambers containing ceramic heat exchange media. The air passes through the ceramic beds (that have been preheated in a previous cycle) and is heated by the stoneware and enters the central chamber at a temperature very close to the incineration temperature. The oxidation process is completed in the central chamber. A gas burner maintains a constant incineration temperature. The maximum fuel use per RTO shall be 50 therms per hours. There shall be no increase in particulate emissions over the inlet conditions.
 - 1. The RTO shall be designed for continuous 24 hours/day, seven days/week throughput of contaminated gas at the following inlet conditions:

a. Air Flow
b. Temperature
c. Humidity
d. THC*
400 ppm average
280 ppm to 512 ppm range

- * The (total hydrocarbons) concentrations are reported as parts per million by volume as propane (C_3H_8) .
- B. The regenerative thermal oxidizer shall be sized and configured to fit into the footprint as shown on the Drawings.

1.07 MAINTENANCE

A. Spare Parts

1. Provide the following spare parts, carefully packed in labeled cartons, tagged with identification of part number, part name, manufacturer and point of use.

Quantity		Description
a.	1	Complete Burner Assemblies
b.	2	Diverter Valves
c.	100 percent	Stoneware for One System
d.	1	Valve Drive Motor
e.	2	Flame Monitors
f.	2	Burner Controllers
g.	1 set	Valve Stems

2. In addition, furnish a list of all spare and replacement parts available for the equipment, with a current price list. The list of prices shall hold firm for the Owner for 1 year.

PART 2 PRODUCTS

2.01 MATERIALS

- A. The energy recovery chambers shall be fabricated from 1/4-in thick ASTM A36 grade steel plate, continuously welded, air tight construction.
 - 1. Each recovery chamber shall be pre-fitted to ensure a trouble free field installation, and pre-insulated with ceramic fiber soft insulation.
 - 2. All recovery chambers shall include a stainless steel ASTM A240, Type 304L stainless steel support grid and gas distribution baffle on the cold face side of the heat recovery bed; and the required quantities of stoneware.
 - 3. The vertically mounted recovery chambers shall sit directly on the foundation to minimize contact points and to provide uniform weight distribution.
- B. The regenerative heat exchanger media shall consist of ceramic matrix saddles, chemically and thermally stable for rapid heat-up for temperatures up to 2300 degrees F.
- C. Each recovery chamber shall have one horizontal tee section, complete with lifting lugs. The tee section shall bolt together to form the combustion chamber. Tee section shall be fabricated from 1/4-in thick ASTM Grade A36 steel plate, continuously welded, airtight construction.
 - 1. Tee section shall be pre-fitted to ensure a trouble-free field installation and preinsulated with ceramic fiber soft insulation.
 - 2. Two controlling thermocouples shall be located in the combustion chamber assembly.
 - 3. The combustion chamber shall be designed to minimize short circuiting between recovery chambers.

- D. All internal insulation shall be ceramic fiber type, modular construction. The insulation shall be a soft, flexible fiber blanket compound with integral stainless steel reinforcement and mounting components.
 - 1. All track work, mounting components, and insulation to be shop installed and fitted prior to shipment.
 - 2. The insulation shall be capable of operating at temperatures up to 2300 degrees F. All parts of the RTO including inlet and outlet ducts, manifolds, etc, which shall have a surface temperature greater than 140 degrees F, shall be insulated to limit the maximum surface temperature to 140 degrees F, at normal operating conditions. All insulation shall be covered with 20 gauge, smooth finish, aluminum jacket.
- E. The inlet manifold shall be fabricated from 12 gauge ASTM A240, Type 304L stainless steel using stainless steel companion angle flanges all welded to the manifold. Access ports for inspection on both sides of the valves and manifolds and expansion fittings shall be provided.
- F. The outlet manifold shall be fabricated from 12 gauge ASTM A240, Type 304L stainless steel, using stainless steel companion angle flanges all welded to the manifold. Access ports for inspection on both sides of the valves and manifolds and expansion fittings shall be provided.
- G. Inlet/Outlet Manifold location Both the Inlet and Outlet manifolds shall be located on the same side of the RTO so that the unit will be located in proper relationship with the process system.
- H. The valve transition shall be fabricated from 12 gauge ASTM A240, Type 304L stainless steel with stainless steel angle reinforcement adequate for the temperatures and pressures involved. Stainless steel angle bracing shall be provided to transfer the load from the manifolds and valves to the foundation.
- I. Diverter valves shall be manufactured with heavy duty cast high temperature steel bodies, stainless steel shaft, solid bushings and shall be metal to metal step-seat butterfly valves.
 - 1. The valves must be capable of operation up to 1,000 degrees F. Leakage shall not exceed more than 0.5 percent at rated airflow, pressure and temperatures.
 - 2. Valves shall be accessible from both sides to facilitate inspection.
 - 3. Valves shall be individually operated by hydraulic, pneumatic or electric actuators. Valves shall be equipped with position proof switches for verification of open and close.
- J. An airflow control system shall be provided to maintain a preset inlet pressure which will automatically control airflow through the oxidizer.
 - 1. The control system shall consist of an AC variable speed drive control (furnished under another Section) for the RTO fan, transmitter and instrumentation to sense and control process exhaust fluctuations.

- K. Two burners at the required rating for each RTO shall be included for maintaining the combustion chamber temperature. The burner shall be designed to operate on natural gas. The burner shall include factory assembled gas train, combustion blower and all required safety features meeting all codes.
 - 1. The burner fuel trains shall include all safeguards, motorized shut-off valves with automatic reset, pressure switches, regulators, test cocks; vent valves, filters, solenoids, pressure reducing valves, pressure gauges required for approval to code.
 - 2. Each burner shall be capable of firing independently and able to provide full combustion chamber heat requirements. Burner combustion blowers shall shut off during normal unit operation to minimize air leakage.

L. Controls Section

1. General

- a. The RTO controls shall provide automatic and semi-automatic startup of each unit. All controls for operation of the RTO and interfaces to completely integrate with the pelletizer control system shall be supplied by the manufacturer. The controls shall have automatic FM approved safety shut-down features, hard wired, in the burner circuitry. All safety controls for the safe operation, or as required by FM, shall be supplied. Individual instrumentation controlling process variables shall be available with an isolated 4-20 mA output signal for remote indication.
- b. All instrumentation required for operation by the manufacturer shall be of the latest revision of the instrument company. All electronic instrumentation shall be of the solid-state type and receive transmission signals generated by thermocouples or 4-20 mA signals generated by other required transmitters. Individual control instruments shall be in accordance with Sections 13301 and 13265.
- c. All recorder readouts shall be linear. Recorders shall be 4 pen, strip chart type by Honeywell or equal.
- d. All field-mounted instrumentation shall be of NEMA 4X design or designed for operation in damp, dusty and slightly corrosive service conditions. All field mounted switches and relays shall be hermetically sealed.
- e. All equipment, cabinets and devices furnished as part of the Contract shall be heavy duty type, designed for continuous industrial service. The system, where practical, shall contain products of a single manufacturer and shall consist of equipment models which are currently in production.
- f. All control equipment shall be designed to operate on 60 Hz, 110 VAC, plus or minus 10 percent, except where specifically noted.
- g. All RTO mounted electrical devices and sensors shall be wired to terminal blocks mounted inside suitable NEMA 4X enclosures.

h. Control Cabinet - A free standing NEMA 12 control cabinet shall be included for each unit and shall be positioned as shown on the Drawings. The cabinet shall be completely prewired using terminal strips within the cabinet. The cabinet shall be tested prior to shipment to minimize any field rewiring.

2. Controlled Parameters

- a. The RTO manufacturer shall supply all controls required or necessary to make a complete and safe functional system.
- b. The flame safeguard shall consist of a FM approved flame interruption device and shall be wired to operate with a continuous or intermittent pilot as mandated by FM for the burner it serves. Flame response time shall be 0.8 seconds. All wiring from the safeguard to the burner train shall be hard wired and independent of the RTO's logic controller. The safeguard shall be wired for non-recycling in the event of flame failure or limit shut-down.
- c. Ultra-violet flame detectors (scanners) shall be utilized.
- d. The temperature sensing elements shall be of the thermocouple type. The type of thermocouple shall be governed by the temperature ranges it will monitor. All thermocouples shall be placed in Type 316 stainless steel thermowells and be long enough to accurately monitor temperature conditions. Thermocouples shall be type J for operation below 1000 degrees F and Type K for above 1000 degrees F. The RTO will be equipped with the following thermocouples as a minimum:
 - 1) Inlet temperature indication
 - 2) Fan inlet temperature shutdown
 - 3) Fan inlet temperature recorder
 - 4) Combustion Chamber temperature shutdown
 - 5) Combustion Chamber temperature #1 burner control
 - 6) Combustion Chamber temperature #2 burner control
 - 7) Combustion Chamber temperature recorder
- e. A pressure sensor transmitter shall be supplied to control the inlet pressure to the RTO. The pressure transmitter operating in conjunction with a controller shall control the RTO fan to maintain a preset draft condition in the inlet duct.
- f. Controllers shall be individually applied to the process variable for which the control is intended. Controllers shall be equal to Honeywell, UDC-3000. All controllers shall be position proportionating-relay output type. No servo amplifiers at the final control device will be accepted. Controllers shall be capable of retransmitting the process variable by way of a 4-20 mA output for remote indication or usage. If required, slave

JOB NO./1096 13267-7

- relays working in conjunction with the controller output contacts shall operate the final control device.
- g. All components of the instrumentation and control system shall be as specified in Section 13265, to assure full compatibility with pelletizing control system.
- M. Fuel Trains The burner fuel trains shall be prepiped and prewired, to terminal strips, within NEMA 3R equivalent enclosures. All instrumentation on the trains shall be of NEMA 4X construction. Pressure switches shall be Honeywell, Mercoid, GE Control Components, or equal. All gas safety valves (2 per burner train) shall be motorized quick starting equal to Maxon series 8000. The gas trains shall be equipped per FM, IRI, and Florida Fuel Gas Code standards. Gas control motors shall be Honeywell 831E. Gas regulators shall be rated for incoming pressure Rockwell; Eaton Corp.; ITT General Controls or equal.

2.03 FABRICATION

- A. The regenerative thermal oxidizers shall be factory built, tested and shipped for installation in the field.
- B. All miscellaneous hardware shall be hot-dip galvanized or stainless steel.

2.04 SURFACE PREPARATION AND SHOP PRIME PAINTING

A. Surface preparation and shop prime painting shall be as specified in Section 09901 and is included in the work of this Section.

PART 3 EXECUTION

3.01 PREPARATION

- A. Coordinate with other trades, equipment and systems to the fullest extent possible.
- B. Take all necessary measurements in the field to determine the exact dimensions for all work and the required sizes of all equipment under this Contract. All pertinent data and dimensions shall be verified by the Contractor.

3.02 INSTALLATION

A. Installation of regenerative thermal oxidizers shall be in strict accordance with the manufacturer's instructions and recommendations in the locations shown on the Drawings. The manufacturer's representative shall supervise the installation of the equipment as required for proper installation.

3.03 PERFORMANCE TESTING

A. The RTO supplier shall conduct performance test (each process train, separately) of the regenerative thermal oxidizers as generally described in the following paragraphs to demonstrate that this subsystem of the overall pelletization system can successfully achieve the mechanical, process and thermal performance requirements set forth in Paragraph 1.06 above.

- B. The RTO supplier shall provide all equipment and supplies necessary to conduct two 8 hour performance tests on each installed RTO, including an accurate means for measuring air flow, temperature, gas flow, particulates and total hydro-carbon concentration as determined by EPA, Method 25A (from 40 CFR), necessary to assess whether or not the RTO meets the specified performance requirements.
- C. All testing shall be the responsibility of the RTO supplier. The laboratory performing the analyses shall be subject to the approval of the Engineer and the Florida Department of Environmental Protection. The RTO supplier shall supply all the necessary equipment and supplies needed to perform the analysis.
- D. If, in the opinion of the Engineer, the system does not meet the parameters of the guaranteed performance test, the RTO supplier shall then have 30 days in which to perform at his/her expense, any supplemental testing, equipment adjustments, changes or additions and request permission to conduct an additional retest of the non-acceptable system. In the event that the equipment does not perform as required, the RTO supplier shall make such modifications that are necessary to achieve compliance or replace the equipment as required all at no additional cost to the Owner. In the event that the equipment meets the mechanical and process requirements but exceeds the thermal efficiency limits, the manufacturer shall pay damages equal to the difference between actual and warranty consumption based on the then current energy rate and 87,600 hours (10 years) for each regenerative thermal oxidizer so deficient.

END OF SECTION

JOB NO./1096 13267-9

Detailed Description of Venturi Scrubber

Detailed Description of Venturi Scrubber

A Detailed Description of a Particular Manufacturer's Venturi Scrubbing System is presented in Appendix M in the O&M Manual of the Envirocare Hydromist Venturipak Wet Scrubber System, Section 1.

SECTION 13262

VENTURI WET SCRUBBER

PART 1 GENERAL

1.01 SCOPE OF WORK

- A. Furnish all labor, materials, equipment, transportation and incidentals required and install, test and make ready for operation the equipment required to remove particulate matter from the sludge processing air stream as shown on the Drawings and as specified herein.
 - 1. Furnish one venturi wet scrubber as part of this Section. The following system components shall be included for each scrubber:
 - a. Venturi wet scrubber, with adjustable damper.
 - b. Cyclonic separator.
 - c. Support structure.
 - d. Spray header with tangential open pipe inlets.

1.02 RELATED WORK

- A. Electric Motors are included in Section 01171.
- B. Refer to Section 11000 for additional specific technical requirements.
- C. Induced Draft Fans are included in Section 15861.
- D. Process Air Ductwork is included in Section 15893.

1.03 SUBMITTALS

- A. Submit, in accordance with Section 01300, shop drawings showing details of fabrication, erection and adjoining equipment interfaces for all equipment furnished under this Section.
- B. Provide manufacturer's rating curves showing pump characteristics of discharge head, capacity, brake horsepower, efficiency, required net positive suction head, and total pumping unit weight. This information shall be prepared specifically for the pumps proposed. Catalog sheets showing a family of curves will not be acceptable.
- C. Provide literature and drawings describing the equipment in sufficient detail, including parts list and materials of construction, to indicate full conformance with the detail requirements.
- D. Provide Sequence of Operations specific to the proposed equipment if it differs from Paragraph 1.07C below.

- E. Provide certified dimensional drawings of each item of equipment and auxiliary apparatus to be furnished
- F. Provide foundation and anchor bolt plans and details.
- G. Provide schematic electrical wiring diagrams and other data as required by the Engineer.
- H. Provide design data, test reports, certificates of compliance, performance curves, particle size verses collection efficiency curves, and warranty data on particulate removal efficiencies.
- I. Provide experience and similar applications list.
- J. Provide welders' qualification certificates, certifying that welders which will be used for all welding procedures comply and meet the quality requirements of ASME Section IX. Provide certified welding procedures which will be used for all welding processes.
- K. Operation and Maintenance Data
 - 1. Provide in accordance with Section 01730, operation and maintenance manuals and equipment start-up reports.
 - 2. Services of a manufacturer's representative shall be provided in accordance with Section 13265.

1.04 REFERENCE STANDARDS

- A. 29 CFR 1926 Safety and Health Regulations for Construction.
- B. American Institute of Steel Construction (AISC)
- C. American Iron and Steel Institute (AISI)
- D. American National Standards Institute (ANSI)
- E. American Society of Mechanical Engineers (ASME)
 - 1. Boiler and Pressure Vessel Code.
 - 2. Code for Pressure Piping B31.3, category D fluid service.
- F. American Society for Testing and Materials (ASTM)
 - 1. ASTM A36 Standard Specification for Carbon Structural Steel
 - 2. ASTM A240 Standard Specification for Heat-Resisting Chromium and Chromium-Nickel Stainless Steel Plate, Sheet and Strip for Pressure Vessels
 - 3. ASTM A276 Standard Specification for Stainless Steel Bars and Shapes

- 4. ASTM A312 Standard Specification for Seamless and Welded Austenitic Stainless Steel Pipes.
- ASTM A320 Standard Specification for Alloy Steel Bolting Materials for Low-Temperature Service.
- 6. ASTM A325 Standard Specification for Strength Bolts for Structural Bolts, Steel, Heat Treated, 120/105 ksi Minimum Tensile Strength.
- 7. ASTM A403 Standard Specification for Wrought Austenitic Stainless Steel Piping Fittings.
- 8. ASTM A480 Standard Specification for General Requirements for Flat-Rolled Stainless and Heat-Resisting Steel Plate, Sheet and Strip
- 9. ASTM A484 Standard Specification for General Requirements for Stainless Steel Bars, Billets and Forgings
- 10. ASTM F593 Standard Specification for Stainless Steel Bolts, Hex Cap Screws and Studs
- 11. ASTM F594 Standard Specification for Stainless Steel Nuts
- G. American Welding Society (AWS)
 - 1. Code D1.1 Structural Welding Code Steel
- H. Underwriters Laboratories (UL)
- I. Environmental Protection Agency (EPA)
 - 1. 40 CFR Part 60, Appendix A
 - a. Method 5; Determination of Point Emissions from Stationary Sources
 - b. Method 9; Visual Determination of the Opacity of Emissions from Stationary Sources
- J. Where reference is made to one of the above standards, the revision in effect at the time of bid opening shall apply.

1.05 QUALITY ASSURANCE

- A. Qualifications The equipment specified under this Section shall be furnished by a manufacturer who is fully experienced, reputable and qualified in the manufacture and assembly of the equipment furnished. Upon request, furnish to the Engineer manufacturer's qualification data including value of like work, locations and references.
- B. Qualifications for Welding Procedures and Operators Comply with the requirements of ASME Boiler and Pressure Vessel Code, "Welding and Brazing Qualification", Section IX.

- C. Provide inspection, examination, and testing in accordance with ASME B31.3 category D fluid service.
- D. Coordinate the interface between the venturi wet scrubber manufacturer and the interfacing equipment. All necessary engineering drawings and details will be furnished to the Engineer.
- E. The venturi wet scrubber and appurtenances shall be manufactured by:
 - 1. Envirocare Systems, Novato, CA
 - 2. Amerex, Inc., Woodstock, GA
 - 3. Clean Gas Systems, Inc., Farmingdale, NY
 - 4. Emtrol Corp., Hauppauge, NY
 - 5. W.W. Sly Manufacturing Company, Cleveland, OH
 - 6. Or equal.
- F. The Contract Documents direct attention to certain required features of this system and equipment, but do not purport to contain all details entering into the equipment design. Furnish and install this equipment complete in all details and ready for operation.

1.06 SYSTEM DESCRIPTION

A. Performance Requirement

- 1. The Venturi Wet Scrubber shall treat the exhaust stream from the tray condenser of the sludge dryer system and achieve a nominal collection efficiency of 96 percent.
- 2. The venturi wet scrubber shall provide removal of fine particulates with a pressure drop no greater than 20-in W.C. at 9,600 ACFM, gas at 180 degrees F with 0.183 pounds water per pound dry air.
- 3. A variable throat damper shall allow adjustment for pressure drop in the range of 15 to 25-in W.C. minimum.

PART 2 PRODUCTS

2.01 SITE CONDITIONS

- A. Maximum Height: 25-ft floor to top of cyclonic separator flange.
- B. Maximum Footprint: 10-ft by 15-ft.
- C. The Drawings and this Section have been based upon the equipment of Envirocare Systems. Equivalent alternative designs manufactured by Amerex, Inc., Emtrol Corp. or equal shall be considered provided that any and all revisions required to the design, including architectural, structural, process piping, instrumentation, plumbing, HVAC and electrical, be accomplished at

JOB NO./1097 13262-4

no additional cost to the Owner. All cost incurred by the Engineer in reviewing the above submittal shall be paid by the Contractor regardless of whether or not the alternative arrangement is accepted.

2.02 MATERIALS

- A. Venturi Scrubber and Cyclonic Separator
 - 1. Exterior structural, shapes and plate
 - a. ASTM A240, Type 304L stainless steel
 - 2. Venturi Throat
 - a. ASTM A240, Type 304L stainless steel
 - 3. Damper and Damper Shaft
 - a. ASTM A240, Type 304 or 304L stainless steel
 - 4. Interior vortex breaker in recirculation tank.
 - a. ASTM A240, Type 304L stainless steel.
 - 5. Bolts, nuts, washers
 - a. ASTM F593, Stainless Steel
 - b. ASTM F594, Stainless Steel
 - 6. Gaskets: Suitable for service
 - a. Neoprene
 - b. Or equal
 - 7. Access doors
 - a. ASTM A240, Type 304 or 304L stainless steel
 - b. Or equal
- B. Exterior Supports
 - 1. ASTM A240, Type 304L stainless steel Supports and stiffeners throughout.
 - 2. ASTM A36 Steel optional on Cyclonic Separator Base only and welded to separator with a poison pad.
- C. Water spray header, inlets and flanged pipe connections.

- 1. Pipe
 - a. ASTM A312, Type 304L stainless steel
- 2. Fittings
 - a. ASTM A403, Type 304L stainless steel
- D. All hardware shall be stainless steel unless otherwise specified.

2.03 FABRICATION

- A. Design and fabricate component sections to minimize field assembling.
- B. Design to minimize deformation and vibration of casing.
- C. Design to fully support section.
- D. Weld gas tight.
- E. Provide lifting lugs, minimum four each section.
- F. Inlet and outlet flanges.
 - 1. Drilled holes to match the mating equipment, breeching and ductwork.
 - 2. Minimum angle size: 3-in by 3-in by 1/2-in.
 - 3. ANSI B16.1, Type 125 lb.
- G. Flue gas connections: round cross section
 - 1. Venturi Scrubber Inlet: 3-ft-6-in ID
 - 2. Cyclonic Separator Outlet: 3-ft-6-in ID

H. Access Doors

- 1. Minimum size 18-in by 15-in rectangular or 20-in round.
- 2. Quick-tightening clamp bolts.
- 3. Gasketed sealing surfaces.
 - a. Acid resistant
 - b. Rated for temperature encountered
 - c. Gastight

JOB NO./1097 13262-6

- 4. Hinges: Size for 200 percent of weight of door.
- 5. Appropriately worded warning signs.
- 6. Locate to clear obstructions when opened.
- I. Pre-assemble all components to assure proper fit upon field assembly.
- J. Disassemble for shipment to minimize damage.
- K. Box non-shop assembled component parts and provide exterior labeling of contents.
- L. Minimize disassembly to minimize field erection.
- M. Maximum shipping weight per shop assembled section, lbs: 8000

2.04 VENTURI SCRUBBER

- A. Housing thickness 3/16-in minimum.
- B. Provide access doors on top and side of flooded elbow above water line to allow for interior inspection and cleaning of venturi.
- C. Drain: 2-in diameter, flanged.
- D. Venturi throat damper
 - 1. Type: Conical, leaf, pivoted plate or butterfly.
 - 2. Variable throat to provide adjustment in pressure drop overall in venturi scrubber and cyclonic separator.
 - 3. Manual handwheel operation.
- E. Venturi spray header.
 - 1. Provide sufficient quantity, size and locations of tangential open pipe water inlets for venturi.
 - 2. All water inlets shall be combined on a single 4-in diameter, flanged spray header.
- F. Air flow shall be in a downward direction.
- G. Provide two 1-in NPT threaded and capped ports at each of the following locations.
 - 1. Inlet to venturi scrubber
 - 2. Flooded elbow section

3. Outlet from Cyclonic Separator

2.05 CYCLONIC SEPARATOR

- A. Housing thickness 3/16-in minimum.
- B. Provide access door on top and bottom above waterline to allow for interior inspection and cleaning of cyclonic separator.
- C. Drain: 4-in diameter, flanged.
- D. Pump Suction: 4-in diameter, flanged.
- E. Overflow: 4-in diameter, flanged.
- F. Transitions:
 - 1. Angle of top cone, maximum: 45 degrees
 - 2. Angle of bottom cone, minimum: 30 degrees

2.06 SUPPORT

- A. Design to support total weight of venturi scrubber, flooded elbow and cyclonic separator filled with water to top of flue gas inlet.
- B. Provide support structure to support from structural floor beams.
- C. Design support structure for all vertical loads.
- D. Provide bracing for horizontal loads.

2.07 PIPING

- A. Provide the flanged connections, headers and tangential open pipe inlets as specified below.
- B. Pipe for use with welded connections shall be manufactured in accordance with ASTM A312 in Type 304L welded stainless steel. Pipe shall be Schedule 10S and manufactured to nominal pipe sizes as listed in ANSI B36.19.
- C. Flanged pipe ends shall be made up of Type 304L angle face rings with hot dipped galvanized ductile iron, back-up flanges with 125 lb drilling pattern.
- D. Fittings for use with welded connections shall be manufactured in accordance with ASTM A403, Class WP-W in Type 304L welded stainless steel. All fittings shall be Schedule 10S, butt weld type.

2.8 SHOP PAINTING

A. Surface preparation and shop prime painting shall be as specified in Section 09901 and is included in the work of this Section.

PART 3 EXECUTION

3.01 PREPARATION

- A. Coordinate with other trades, equipment and systems to the fullest extent possible.
- B. Take all necessary measurements in the field to determine the exact dimensions for all work and the required sizes of all equipment under this Contract. All pertinent data and dimensions shall be verified by the Contractor.

3.02 INSTALLATION

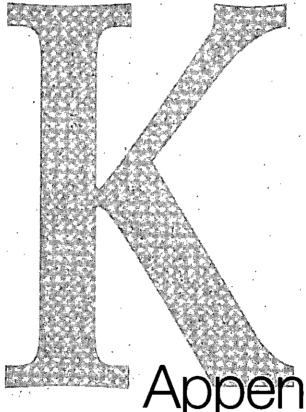
- A. All equipment shall be installed in accordance with the instructions of the manufacturer and as shown on the Drawings.
- B. During installation and before the plant equipment is placed in operation, the manufacturer shall inspect and prepare a detailed Inspection and Testing Report which certifies that all units and accessories have been properly installed, adjusted and made ready for operation, all by a qualified representative at no additional cost.
- C. All angle face ring joints for piping shall be cleaned interior and exterior, of all welded spatter, stains and sharp edges after fabrication. Butt welded joints require only exterior cleaning.
- D. Field tests shall not be conducted until such time that the entire installation is complete and ready for testing.
- E. All adjustments necessary to place the equipment in satisfactory working order shall be made at the time of the above tests.

3.03 FIELD TESTS

- A. Perform visual examination as specified in ASME B31.3 for piping. Replace or repair defective components and workmanship until the acceptance criteria is met at no additional cost to the Owner.
- B. Perform air leakage and hydrostatic tests. The Engineer shall be given a 7 day notice to witness test operations.
- C. Provide all equipment and supplies necessary to conduct a performance test on each installed venturi wet scrubber including an accurate means for measuring air flow, temperature, humidity and particulate concentration and other apparatus necessary to assess whether or not the system meets the performance requirements specified in Paragraph 1.06 above. The schedule of the performance test shall be subject to the approval of the Engineer. Prior to the performance test, submit a plan of all work, measurements and details of the performance test to the Engineer for approval. All testing will be the responsibility of the Contractor. The laboratory or person performing the analysis shall be subject to the approval of the Engineer. Supply all the necessary equipment and supplies needed to perform the analysis. A laboratory certified by the State of Florida shall be used to perform the analysis.
- D. If, in the opinion of the Engineer, the system does not meet the warranty, the Contractor shall then have 30 days in which to perform at the Contractor's expense, any supplemental testing, equipment adjustments, changes or additions and request an additional retest of the non-acceptable system.
- E. If, after a second and final test, the equipment fails to meet the performance requirements, remove and replace the venturi wet scrubbers with equipment that meets the performance requirements at no additional cost to the Owner.

END OF SECTION

JOB NO./1097 13262-10



Appendix K



Appendix K
Description of Stack Sampling Facilities

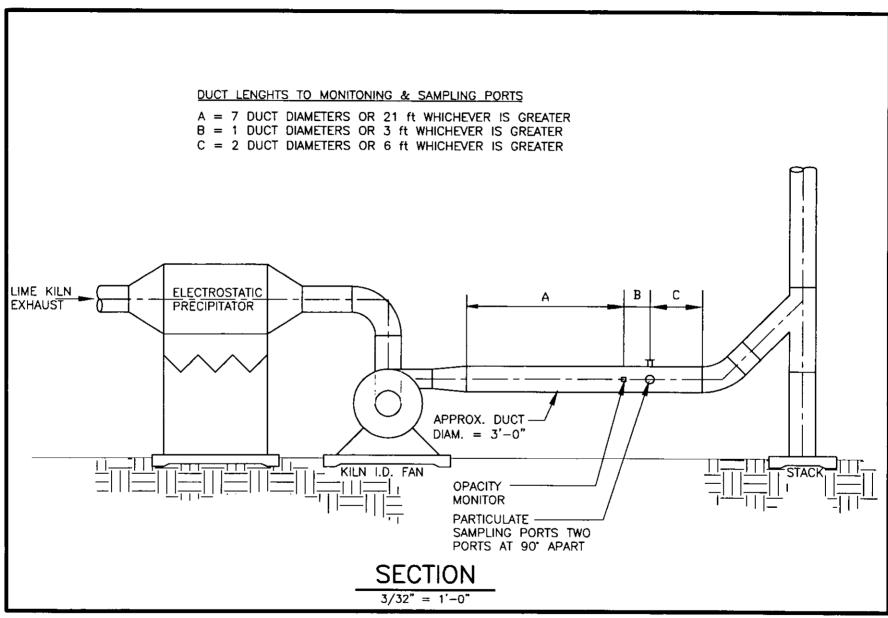


Figure No. K-1 Location of Opacity Monitor and Particulate Sampling Ports on Lime Recalcination Facility

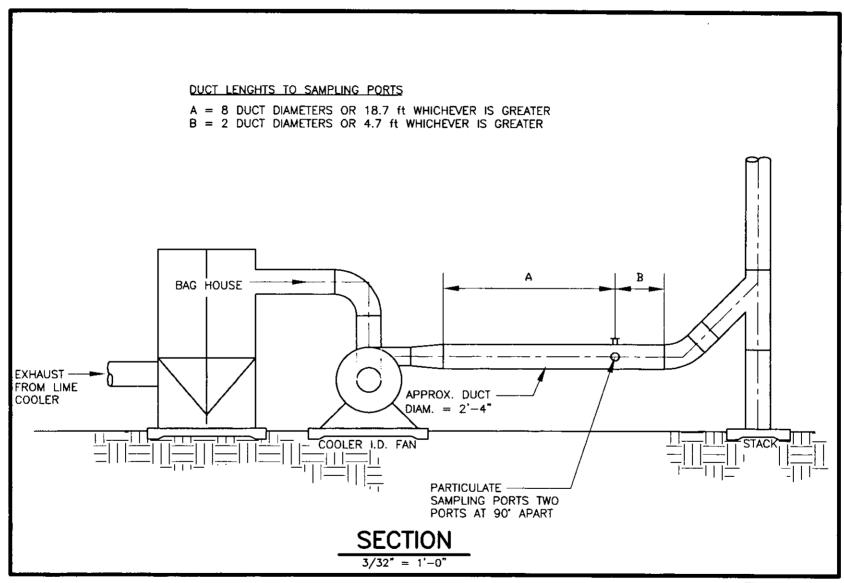
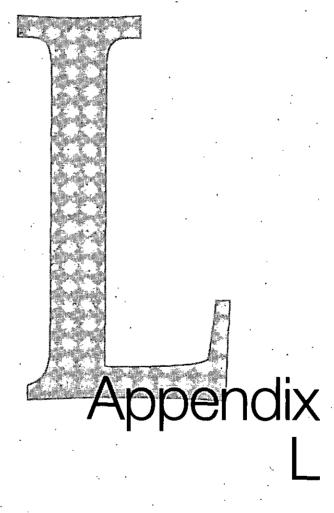


Figure No. K-2 Location of Sampling Ports on Lime Cooler Stack at Lime Recalcination Facility

FIGURE-K-3

Figure No. K-3 Location of Particulate Sampling Ports on Biosolids Pelletization Facility



Appendix L Start-up, Shutdown and Malfunction Conditions

Appendix L Startup, Shutdown and Malfunction Conditions

This appendix describes the operating conditions during which excess air emissions can occur: startup, shutdown and malfunction conditions of the Lime Recalcination Facility (LRF) and Biosolids Pelletization Facility (BPF). Measures to control these emissions, and proposed permit conditions for the startup, shutdown and malfunction periods are also discussed.

L.1 Startup, Shutdown and Malfunction Conditions for the LRF

L.1.1 Introduction

It is generally recognized that air pollutant emissions from a lime kiln facility are lowest when the facility is operated at steady state conditions with all components of the system (i.e. kiln, lime sludge feed system, burner train, product conveying and cooling system, air pollution control equipment, ID fan, etc.) are on line. Periods of warm-up, start-up, shutdown and malfunction are unstable, transitory in nature and usually outside the normal operating range of the equipment. Therefore, these periods warrant special consideration from an air emissions and permitting standpoint. This fact is noted in the following excerpt from the general provisions of the New Source Performance Standards (NSPS) (40CFR, Part 60, 60.8, c).

Operations during periods of startup, shutdown, and malfunction shall not constitute representative conditions for the purpose of a performance test nor shall emissions in excess of the level of the applicable emission limit during periods of startup, shutdown, and malfunction be considered a violation of the applicable emission limit unless otherwise specified in the applicable standard.

The North County Resource Recovery Facility (NCRRF) Site's current Title V Air Operating Permit allows air emission excursions up to three hours in duration per occurrence during periods of startup, shutdown, and malfunction at the NCRRF before the excursion is considered a permit violation. SWA requests that this same three-hour excursion be applied to startup, shutdown and malfunction periods at the BPF and LRF.

L.1.2 Exclusionary Periods

Based on the above, the following exclusionary periods are defined for the LRF:

Warm-up – Warm-up are those periods in which landfill or natural gas is being fired in the kiln and the kiln is being brought up to (or being maintained at) operating temperature, but no lime sludge is being fed to the kiln.



Startup – Startup is the period beginning with the feeding of lime sludge into the kiln and ending when steady state operation is achieved. It takes approximately 12 hours from when lime first enters the kiln to when steady state conditions are achieved.

Shutdown – Shutdown is the period starting when the feeding of lime sludge into the kiln stops (with the intention of bringing the unit down) to when the last of the lime product leaves the kiln and the lime product cooler. Shutdown can be expected to take up to approximately six hours.

Cool Down – Cool down is the period following shutdown during which the temperature of the kiln is gradually lowered to near ambient conditions. Cool down starts when the last of the lime product leaves the kiln and the product cooler to when the kiln burner and fan are turned off. During cool down the kiln burner may be on low fire for extended periods of time to allow the kiln to slowly cool.

Malfunction or Upset – A malfunction is any sudden and unavoidable failure of air pollution control equipment or process equipment to operate in a normal and usual manner. The term "malfunction" does not apply to operator error, poor maintenance, poor operation, or any other equipment or process upset that can reasonably be prevented. A malfunction or upset condition can occur due to an equipment trip or failure. Some equipment outages are minor and can be fixed relatively quickly while the facility is still in operation. Other more serious outages will require immediate shutdown of the process and repair of the faulty component.

L.1.3 Air Emissions During Exclusionary Periods

Based on the current Title V Operating Permit conditions for the NCRRF, the following permit conditions for the LRF are proposed:

- 1. During periods of Warm-up and Cool Down (when no lime sludge is being fed to the kiln), the facility is not be considered to be in operation, so the particulate matter and opacity limits from 40 CFR 60 Subpart HH (Lime Manufacturing NSPS) would not apply. However, the non-methane organic compound control requirement from 40 CFR 60 Subpart WWW (Landfill Gas NSPS) would apply to the burning of landfill gas during these periods. In addition, the ESP would come on-line, and be hot and ready during the Warm-up, and would be kept operating during Cool Down.
- 2. During periods of Startup and Shutdown (as defined above), air emission excursions above permit emissions limits of up to three hours per occurrence would be allowed. The electrostatic precipitator (ESP) on the kiln exhaust, and the baghouse on the lime cooler exhaust, would be operating during Startup and Shutdown, and all air emissions would pass through one of these two control devices.



3. During periods of Malfunction, air emission excursions of up to three hours per occurrence would be allowed for each equipment malfunction. Particulate matter emissions would be controlled by the ESP or the lime cooler baghouse, unless the malfunction were to the air pollution control equipment itself (see Section L.1.5, below). Consistent with the requirements of SWA's Power Plant Siting Conditions of Certification, No. PA-84, Section III., SWA will report to the Florida Department of Environmental Protection (FDEP) Southeast District any malfunctions that "compromise the integrity of the operation", any air pollution control equipment malfunctions exceeding two hours, and any continuous opacity monitor malfunctions exceeding four hours.

L.1.4 Operational Sequences

The following section briefly describe the operational sequences which occur during warm-up, startup, shutdown, cool down and malfunction periods.

Warm-Up

A warm-up begins with starting of the ID fan to establish air flow through the system. Then the kiln burner is lit and the kiln is rotated and gradually brought up to operating temperature. Heating up of the kiln should be done slowly at the rate of about 100 degrees per hour to allow the bricks to expand evenly. Towards the end of the warm-up period, the kiln ESP is energized, and the product conveying and cooling equipment (cross-bar cooler, cooler blower and ID fan, and the cooler baghouse) are started. Then the feeding of lime sludge to the kiln can begin.

Start-Up

Start-up begins with the feeding of lime sludge to the kiln. As the feed rate of lime sludge is gradually increased, the rate of fuel firing to the burner will gradually increase. From the time lime sludge is first introduced into the kiln, it will take approximately 12 hours for the kiln to reach a steady state operating condition.

Shutdown

The general procedure for shutdown will be to stop the feeding of lime sludge to the kiln but continue firing fuel to the kiln burner until the kiln is clear of lime. The shutdown procedure is expected to take up to six hours after the feeding of lime sludge has stopped. During shutdown the burner firing rate will gradually decrease as the last of the lime sludge is discharged from the kiln. Also, during shutdown the last of the lime product is being cleared from the product cooling and conveying equipment.

Cool Down

Once the kiln is clear of lime, the kiln burner can be set to a lower firing rate to allow the kiln to slowly cool down to ambient conditions. Cool down, like warm-up, is done slowly to allow the bricks to gradually adjust to the changing temperature without thermally shocking the refractories. Usually a full cool down to ambient conditions is



only done when an internal inspection or repair of the kiln refractories is required. In other instances, necessary repairs can be made during the cool down period and a restart (or warm-up) of the equipment can begin. The ESP and lime cooler baghouse will be shut down sometime during this period.

Malfunction

In general, only the equipment which experienced the trip or malfunction will need to be restarted. The severity of the equipment trip or malfunction will dictate whether just the tripped equipment can be quickly restarted, or whether the kiln burner and lime feed systems must be shut down and the upset condition corrected before a restart can be initiated.

L.1.5 Malfunctions

The following section describes the type of malfunctions that can be expected to occur. Malfunctions can be classified into four categories: kiln malfunctions, air pollution control malfunctions, lime feed or product conveying malfunctions and miscellaneous malfunctions.

Kiln Malfunctions

Kiln malfunctions include loss of burner train, ID fan, kiln motor or gear drives. Also under rare circumstances a dam or ring can form in the kiln damming up the flow of lime through the kiln. The dam must be removed for the operation to continue. Depending on the severity of the malfunction, the problem can either be fixed with the system staying on-line or the kiln must be shut down and the problem corrected before operation is resumed.

Air Pollution Control Equipment Malfunctions

Malfunctions in this group typically consist of loss of a field in the ESP, broken bags in the cooler baghouse, or loss of the baghouse pulsed air cleaning system. Some of these malfunctions can be quickly fixed (such as a trip of a transformer/rectifier on one of the ESP fields), in which case it would not be worth shutting down the whole system to correct the problem. For any other malfunctions that could take more than three hours to repair, the kiln burner and feeds to the system will be shut down while the malfunction is corrected.

Lime Feed and Product Conveying Malfunctions

For the lime feed systems, malfunctions include failures of the lime sludge receiving, blending, storage, pumping, dewatering and conveying equipment. Many of these systems have redundant units (i.e. two sludge pumps, two dewatering centrifuges, etc.) so that shut down of the system can be avoided. However, for product conveying, there is only one product cooler and if it gets jammed with a large chunk of lime or its blower or ID fan fail, then shutdown the kiln burner and stopping all feeds to the kiln will be required if the problem cannot be corrected within three hours.



Miscellaneous Malfunctions

Miscellaneous malfunctions are related to equipment and processes not directly tied to the kiln, air pollution control, lime mud or product feed systems. These typically include: loss of electrical power from the power grid, loss of the landfill gas pressurization or refrigeration systems, or insufficient supply of landfill gas. The kiln will have natural gas as a backup fuel so that problems with the landfill gas supply or preparation systems should not cause a shutdown of the lime kiln.

L.2 Start-up, Shutdown and Malfunction Conditions for the BPF

L.2.1 Introduction

Similar to the LRF, air pollutant emissions from the BPF are lowest when the facility is operated at steady-state conditions with all components of the system (i.e. furnace, dryer, wet sludge feed systems, product handling and conveying systems, air pollution control equipment, condenser and cooling tower, ID fan, regenerative thermal oxidizer (RTO), etc.) on line. Periods of warm-up, startup, shutdown and malfunction are unstable, transitory in nature and usually outside the normal operating range of the equipment. Therefore, these periods warrant special consideration with respect to air emissions limits, and apply to each of the two dryers at the BPF.

L.2.2 Exclusionary Periods

The following exclusionary periods are defined for the BPF:

Warm-up - Warm-up are those periods in which landfill or natural gas is being fired in the dryer furnace and the system is being brought up to (or being maintained at) operating temperature, but no biosolids are being fed to the dryer.

Startup – Startup is the period beginning with the feeding of biosolids into the dryer and ending when steady state operation is achieved. It takes approximately six hours from when biosolids first enter the dryer to when steady-state conditions are achieved.

Shutdown – Shutdown is the period starting when the feeding of biosolids into the dryer stops (with the intention of bringing the unit to cool down) to when the last of the biosolids product leaves the dryer and product cooler. Shutdown can be expected to take up to approximately three hours.

Cool Down - Cool down is the period following shutdown during which the temperature of the dryer, dryer furnace and RTO are gradually lowered to near ambient conditions. Cool down starts when the last of the biosolids product leaves the dryer and product cooler to when the dryer and RTO burners, ID fan and RTO exhaust fan are turned off. During cool down the dryer and RTO burners may be on low fire for extended periods of time to allow the dryer furnace and RTO to slowly cool.



Malfunction or Upset – A malfunction is any sudden and unavoidable failure of air pollution control equipment or process equipment to operate in a normal and usual manner. The term "malfunction" does not apply to operator error, poor maintenance, poor operation, or any other equipment or process upset that can reasonably be prevented. A malfunction or upset condition can occur due to an equipment trip or failure. Some equipment outages are minor and can be fixed relatively quickly while the facility is still in operation. Other more serious outages will require immediate shutdown of the process and repair of the faulty component.

L.2.3 Air Emissions During Exclusionary Periods

Based on the current Title V Operating Permit conditions for the NCRRF, the following permit conditions for the BPF are proposed:

- 1. During periods of Warm-up and Cool Down (when no biosolids are being fed to the dryer), the facility is not considered to be in operation and air emission limits would not apply. Only the non-methane organic compound control requirement from 40 CFR 60 Subpart WWW (Landfill Gas NSPS) would apply to the burning of landfill gas during these periods. The air pollution control equipment (tray condenser, venturi scrubber, and RTO) would come on-line during Warm-up, and remain operational until Cool Down.
- During periods of Startup and Shutdown (as defined above), air emission
 excursions above permit emissions limits of up to three hours per occurrence
 would be allowed. The tray condenser, venturi scrubber, and RTO would be
 operating during Startup and Shutdown, and all exhaust gases would go
 through these control devices.
- 3. During periods of Malfunction, air emission excursions of up to three hours per occurrence would be allowed for each equipment. Air emissions would be controlled, unless the malfunction were with the tray condenser, venturi scrubber or RTO (see Section L.2.5, below). Consistent with the requirements of SWA's Power Plant Siting Conditions of Certification, No. PA-84, Section III., SWA will report to the FDEP Southeast District any malfunctions that "compromise the integrity of the operation", and any air pollution control equipment malfunctions exceeding two hours.

L.2.4 Operational Sequences

The following sections briefly describe the operational sequences which occur during warm-up, startup, shutdown, cool down and malfunction periods.

Warm-Up

A warm-up begins with the starting of the ID fan to establish air flow through the system. Then water flow through the tray condenser, venturi scrubber and cooling tower is started. Next the RTO is brought on line by starting its burners and exhaust fan. The dryer drum is then rotated, the dryer burner is lit, and the system is brought



up to operating temperature. The product handling and conveying equipment (vibrating screen, crusher and numerous screw conveyors and bucket elevators) are then started. The feeding of sludge to the kiln can then begin.

Startup

Startup begins with the feeding of biosolids into the dryer. As the feed rate of biosolids is gradually increased, the rate of fuel firing to the burner will gradually increase. From the time sludge is first introduced into the dryer, it will take approximately six hours for the dryer system to reach a steady state operating condition.

Shutdown

The general procedure for shutdown will be to stop the feeding of biosolids to the dryer but continue firing fuel to the dryer burner until the dryer and product conveying and cooling systems are clear of biosolids. As the biosolids are cleared from the system, the burner firing rate will gradually decrease. Once the product handling and conveying systems are cleared of biosolids, these systems can be shut down. The shutdown procedure is expected to take approximately six hours after the feeding of biosolids has stopped. The air pollution control equipment will continue to operate during shutdown.

Cool Down

Once the system is clear of biosolids, the dryer burner and RTO burners are set to low firing rates to allow the dryer, dryer furnace and RTO to gradually cool down to ambient conditions. Once these systems have sufficiently cooled, the dryer and RTO burners can be turned off, the dryer ID fan and RTO exhaust fan shut down, and the water flows to the condenser, venturi scrubber and cooling tower shut down.

Malfunction

In general, only the equipment which experienced the trip or malfunction will need to be restarted. The severity of the equipment trip or malfunction will dictate whether just the tripped equipment can be quickly restarted or whether the dryer burner and biosolids feed systems must be shut down and the upset condition corrected before a restart can be initiated.

L.2.5 Malfunctions

The following section describes the types of malfunctions that can be expected to occur. Malfunctions can be classified into four categories: dryer malfunctions, air pollution control malfunctions, sludge feed or product conveying malfunctions and miscellaneous malfunctions.

Dryer Malfunctions

Dryer malfunctions include loss of burner train, ID fan, dryer drum motor or gear drives. Depending on the severity of the malfunction, the problem can either be fixed



with the system staying in operation or the dryer must be shut down and the problem corrected before operation is resumed. Loss of the dryer ID fan is a serious malfunction which would require immediate shutdown of the system.

Air Pollution Control Equipment Malfunctions

Malfunctions in this group typically consist of loss of water flow to the condenser, venturi scrubber or cooling tower, a blockage in the polycyclone or venturi scrubber, or loss of the RTO or its exhaust fan. Some of these malfunctions can be quickly fixed (such as a trip of one of the water pumps) and thus it would not be worth shutting down the whole system to correct the problem. For any other malfunctions that could take more than three hours to repair, the dryer burner and feeds to the system would have to be shut down to correct the problem.

Biosolids Feed and Product Handling/Conveying Malfunctions

Malfunctions of the biosolids feed systems could include failures of the biosolids receiving, conveying and feeding equipment (live bottom hoppers, screw conveyors, bucket elevator and pug mill mixer). Many of these systems have redundant units (i.e. each dryer has two live bottom hoppers, two bucket elevators with associated screw conveyors, etc.) so that shut down of each dryer system can be avoided. However, for product cooling and conveying, there is only one set of equipment per dryer, and if one component of this equipment gets jammed, then stopping the biosolids feed to the effected dryer will be required if the malfunction cannot be corrected within three hours.

Miscellaneous Malfunctions

Miscellaneous malfunctions are related to equipment and processes not directly tied to the dryer, air pollution control, biosolids feed or product handling systems. These typically include: loss of electrical power from the power grid, loss of the landfill gas pressurization or refrigeration systems, insufficient supply of landfill gas. The dryers will have natural gas as a backup fuel so that problems with the landfill gas supply or preparation systems should not cause shut down of the BPF.



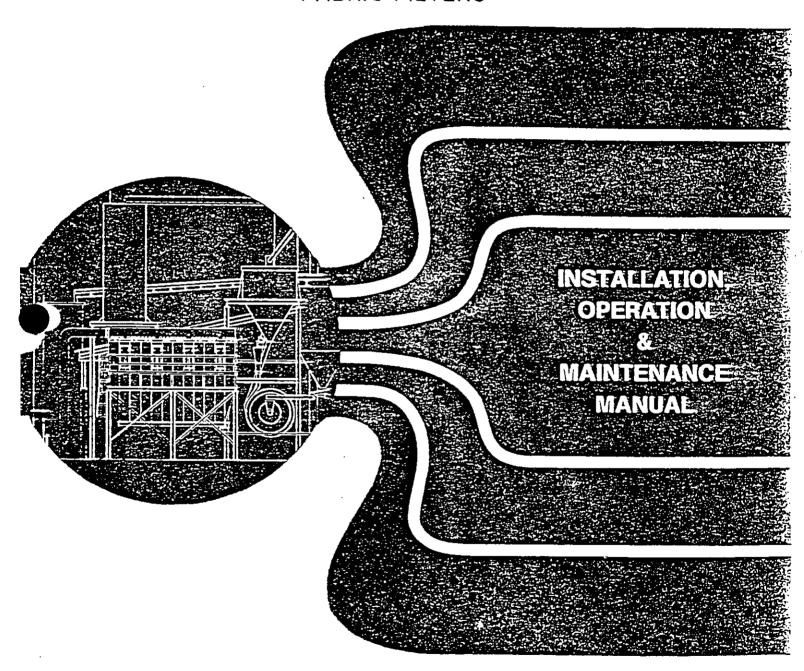


Appendix M Operations and Maintenance Plans Operation and Maintenance Manual for Baghouse on Lime Cooler Exhaust

Operations and Maintenance Manual for Baghouse On Lime Cooler Exhaust

FABRI-JET™ & ULTRA

FABRIC FILTERS



ULTRA INDUSTRIES INC.

FABRIC FILTER DIVISION

OPERATING PRINCIPLES

FABRI-JET™ and ULTRA dust collectors remove 99.9% of dust particles quickly, efficiently. Units operate by this simple method:

Dust-laden air enters the hopper where heavier particles drop out of the air stream. Lighter particles are trapped in the air stream and rise.

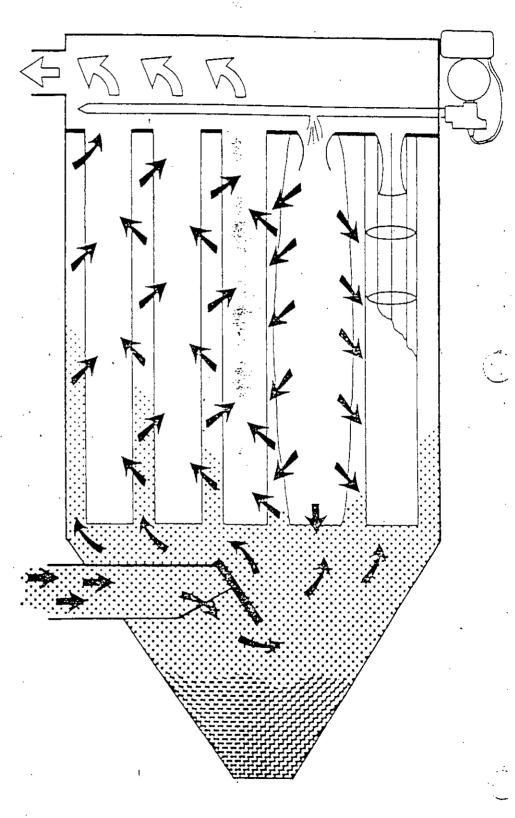
As the air passes through the filter bags, dust particles are collected on the outside surface of the filter bags and the cleaned air is exhausted from the collector.

At precise intervals, jets of high pressure air pass through the venturis, inducing a strong flow of secondary air, briefly reversing the air flow through the bags.

Shock waves pass down the inside of the bags, flexing the bags outward. The reversed air flow dislodges accumulated dust from the bag and the dust drops into the hopper.

With this method of cleaning, airflow through a row of bags is reversed for only a fraction of a second, resulting in steady airflow through the collector. The system is therefore maintained at steady-state conditions.

Collection operation is controlled by an easily-adjusted solid state timer. A Magnahelic gauge permits optimum regulation of the timer. Pulse durations and pulse intervals can be simply and accurately set at the timer to minimize air consumption.



RECEIVING YOUR COLLECTOR

Congratulations on selecting a FABRI-JET™ or ULTRA collector for state of the art, efficient, thorough air pollution control and product recovery. We urge that you read and follow the instructions and advice which follow. We want you to be thoroughly satisfied with your collector.

- 100 mm - 1

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SHIPMENT

FABRI-JET™ and ULTRA collectors have been designed to minimize customer assembly. Air headers, solenoids, air piping and air pressure gauges are all shipped mounted on the collectors, completely piped for operation.

Housings for the FABRI-JETM and ULTRA Models BB, CB, CF and SQ collectors are shipped as completey welded assemblies. Larger rectangular collectors are shipped in two subassemblies. The hopper is often inverted and nested inside the main housing. Walk-in plenums for top bag removal collectors are shipped as a separate subassembly.

Timers, bags, bag clamps, cages and differential pressure gauges are shipped separate from the collector. These shipments are carefully marked for identification.

∴ INSPECTION

FABRI-JET^M and ULTRA collectors are carefully inspected before shipment to ensure high quality workmanship. Heavy skids and secure truck cribbing are used but at times damages do occur during shipment. We recommend that you inspect your collector when it is received for any possible damage — if there is any damage or a shortage, it should be noted on your bill of lading. Purchaser should file claims against the carrier within a few days of receipt of the shipment. Damage incurred in transit is the responsibility of the common carrier. Since it is the manufacturers policy to ship F.O.B. the factory, any claims must be initiated against the carrier by the purchaser.

STORAGE

The standard finish for the outside of the collector is one coat of factory primer, unless additional finish coats or special coatings were specified.

If additional protection is required because of lengthy outside storage, corrosive atmosphere or other conditions, the collector should be given an additional protective coat while the prime coat is in good condition.

Bags and cages, which will arrive in a separate shipment to avoid shipping damage, should be stored in a dry, indoor location.

MOUNTING THE DIFFERENTIAL PRESSURE GAUGE

INSTALLATION All accessories and a detailed instruction sheet are packed in the box with your gauge.

LOCATION Mount the gauge in a location that is free from excessive vibration and where the temperature does not exceed 140°F. Avoid direct sunlight.

CONNECTING GAUGE For a permanent installation it is recommended that ¼ " O.D. copper tubing be used with regular compression fittings. An in-line paper filter will prevent dust from getting into the gauge line. If this is not used, it is recommended that a loop be placed in the high pressure line that leads from the dirty air housing so that dust does not enter the gauge.

Adjust the differential pressure gauge to indicate zero.

INSTALLING THE COMPRESSED AIR CLEANING SYSTEM

AIR CONSUMPTION The average amount of air that is consumed is listed on the drawing for each collector. This is based on a six second pulse interval, "OFF-TIME", and a pulse duration of .05 seconds, "ON TIME", which are average settings for most applications and can be varied up or down depending on the type of dust and dust loading. For example with a very light dust loading the "OFF TIME" could be set at 12 to 18 seconds thus reducing the air requirements to ½ or ½ of the stated volume. A corresponding reduction in the size of the air supply piping may be made.

AIR SUPPLY PIPING A 1" to 2½" O.D. compressed air supply pipe furnishing 85 to 100 psig air (whether all or no other equipment on the same line is used) should be connected to the air header. Refer to RECOMMENDED PIPE SIZES table below. Higher pressures shorten bag life, lower pressures do not adequately clean the filter bags. It is good practice to blow down the air supply piping before connecting it to the air header. This removes any debris in the supply pipe before it is connected to your collector.

AIR QUALITY Dirt, scale, or foreign matter in the piping can cause problems of the air pulsing system. Oil in the air supply can eventually cause plugging of the bags. Water in the system can cause valve problems plus the chance of freeze-up in a cold atmosphere. It is, therefore, necessary that the air be clean, dry and oil-free. The air receiver should have an automatic moisture drain. In-line air filters with automatic drains may suffice if moisture content is not too great and if kept from freezing. However, if a large amount of moisture or oil is present, a desiccant-type filter is recommended.

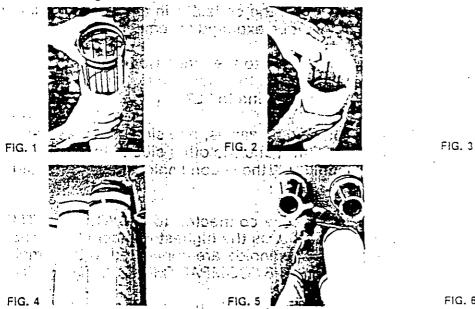
RECOMMENDED PIPE SIZES

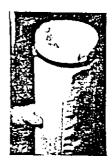
Total free air consumption	Up to 100 ft.	Up to 500 ft.	Up to 1,000 ft.
up to 50 SCFM	1" O.D.	11/4 " O.D.	1¼″O.D.
51 to 100 SCFM	11/4 " O.D.	1 ½ ″ O.D.	2" O.D.
101 to 200 SCFM	1½" O.D.	2" O.D.	2½″ O.D.

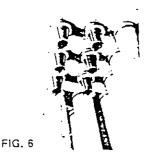
INSTALLING THE FILTER BAGS

SIDE BAG REMOVAL COLLECTORS

- 1. Slip filter bag over the cage, making sure that the bag seam is not over the split in the p collar of cage. (See Fig. 1.)
- 2. Bottom of bag must be tight against the cage bottom, the seam should be straight and all wrinkles smoothed out.
- 3. Fold the top of the bag (about two inches) over the top of cage, smooth out the inside folds, and make sure that bag does not overlap the annular groove on inside of cage (trim off excess bag length if necessary). (See Fig. 2.)
- 4. Slip on the bag clamp (loosely). The tightening mechanism should not be over the bag seam. (See Fig. 3.)
- 5. Slide the bag and cage upward over the bag cup until the cage snaps into place on the groove in the bag cup. Bag and cage assembly should fit tight against tubesheet for proper alignment. (See Fig. 4.)
- 6. Tighten bag clamp. It is important that a %" socket be used: a screwdriver may slip and puncture the bag. (See Fig. 5.)
- 7. Check to make sure that bags are hanging straight, and do not touch other bags or the collector housing. (See Fig. 6.)
- 8. Install the remaining bags in the same manner.
- 9. Close and tighten; all access doors.





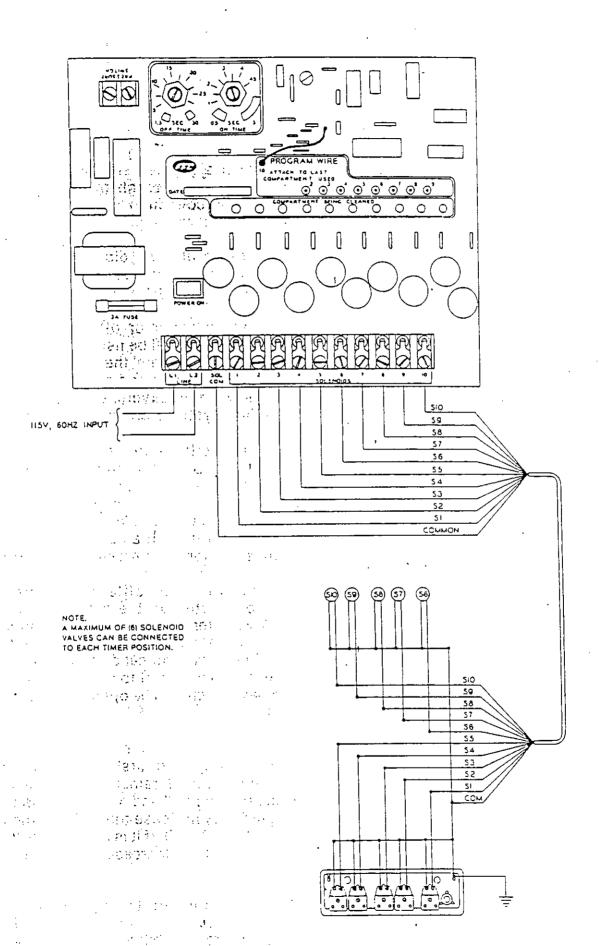


TOP BAG REMOVAL COLLECTORS

- 1. From the top side of the tubesheet, lower the bag into the housing up to the bag cuff.
- 2. The bag cuff has two sewn-in steel bands. Collapse the cuff into a U-shape and lower the bag until one of the bands is below the tubesheet and one above. Then let the cuff spring back to its original shape. Smooth the cuff around the hole. The cuff should form a perfect seal at the tubesheet.
- 3. Lower the cage assembly into the bag and press firmly into place.
- 4. Install the remaining bags in the same manner.
- 5. Locate a blowpipe over each row of bags and connect each blowpipe to the air header by slipping the blowpipe into the coupling at the collector wall and tightening the collar.
- 6. Close and tighten all access doors.

INSTALLING THE SOLID STATE TIMER

- 1. The FABRI-JET™ and ULTRA timer is a completely solid state switching unit manufactured to rigid specifications. The timer is capable of switching up to 10 outputs at 1 amp each with 115 volts line input. Each output is capable of handling one solenoid on each air header and can handle up to six headers for a total of sixty solenoids, i.e. sixty rows of filter bags per timer.
- 2. The timing range is fully adjustable for optimum collector performance. The "ON TIME" (pulse duration) is adjustable from .05 seconds to .5 seconds. The "OFF TIME" (interval between pulses) can be varied from 1.5 to 30 seconds. An indicator light for "power on" is prominently located on the board as well as lights which indicate which row of bags is being cleaned. If desired, the timer can be activated by an external differential pressure switch. In this arrangement the cleaning cycle would be used only when it is necessary, as determined by a preset pressure drop across the tubesheet.
- 3. The standard timer is shipped in a NEMA 4, weatherproof enclosure for mounting by the customer. Other enclosures are available for hazardous applications.
- 4. If the timer is to be mounted on the collector, vibration mounts should be provided. It is more desirable to mount the timer away from the collector in an accessible location that is free from vibration. The timer should not be exposed to temperatures over 120°E.
- 5. Install an "ON-OFF" switch in the power supply to the timer. Connect 115 volt, single phase, 60 Hz, 10 amperes input through this switch to timer terminals marked "Line L1" and "L2". In grounded systems connect neutral of line to "L2".
- 6. Connect wiring between the timer and solenoid valves; one side of each solenoid to the timer common terminal marked "SOL COM.", and the other side of the first solenoid to the timer output terminal marked "Solenoids 1", the second solenoid to "Solenoids 2", etc.
- 7. The black program wire in the timer should be connected to the "COMPARTMENT USED" socket number which is the same number as the highest numbered "Solenoids" terminal which is used. For example: if eight solenoids are connected to the timer, the program wire should be connected to the number 8 "COMPARTMENT USED" socket.
- 8. On collectors with more than one air header, one wire from each solenoid is connected to the timer terminal marked "SOL COM." The other wire from the first valve on each header should be connected to the timer terminal marked "Solenoids 1", the second valve on each header to "Solenoids 2", etc. On certain collectors the number of solenoid valves on each header differ. For example: a collector may have a total of 26 valves with three air headers. Two would have 9 valves, the third 8. The solenoids would be connected in sequence to the timer, with three wires on positions one through eight. On the ninth post there would be only two solenoid wires. The program wire would be connected to the ninth "COMPARTMENT USED" socket.



INITIAL SYSTEM START UP

AUXILIARY EQUIPMENT

Inspect all equipment before start-up to see that there are no foreign objects in rotating equipment and that safety equipment is in place.

Start the fan, screw conveyor and/or airlock and inspect for proper rotation and that all equipment runs smoothly. After making the necessary corrections turn all this equipment off.

DUCTWORK

See that all connections are tight and that all cleanout ports are closed. The ductwork must be free of debris.

STARTING SYSTEM

- 1. All doors and ports should be closed, with timer and auxiliary equipment off. Turn on compressed air to collector and inspect the system for leaks. If air is leaking from any blowpipe with the timer off there may be a leak between its solenoid and diaphragm valve. Inspect the ½ " O D tubing between the solenoids and diaphragm valves to be certain that all connections are tight and there are no leaks. The tubing must not be crimped. Shut off compressed air supply.
- 2. Turn on timer. The red "power on" indicator should light. Turn "OFF TIME" and "ON TIME" knobs fully counterclockwise. The individual timing lights should blink at 1.5 second intervals and the corresponding solenoid valves will be activated (audible).
- 3. Turn on the air supply to the air header. All solenoid valves should be operating and the exhaust air from each valve can be felt.

Let the collector pulse for ten minutes to clear all lines then set "OFF" time to between six to ten seconds with 85 psig air supplied. Later this may be adjusted to suit your collection requirements based on the dust loading.

- 4. Turn on all dust discharge equipment such as rotary valves, screw conveyors, etc.
- 5. If water vapor or other condensables are present, it will be necessary to preheat the system so that the surface temperature of the piping and collector are above the dew point. Dryers, coolers and some grinding systems are common examples.
- 6. Start the fan with the fan damper set at about half-flow and run for 30 minutes because it is good practice to introduce the dust stream to a new bag at a reduced rate. This is particularly true when very fine solids (less than 2 microns) or high concentrations are present.
- 7. Observe the differential pressure gauge. At start-up the pressure drop will be low. After 30 minutes of operation the bags will start to be coated, the filtering efficiency will increase and the pressure differential will start to rise. Then the main fan damper should be opened to the design setting.
- 8. When the collector has stabilized (may require eight hours) the differential pressure should remain steady at some value between 1" and 6" W.G. If it is below 4" gradually increase the "OFF" time until it reaches 4" W.G. If it is over 4" the "OFF" time should be decreased until it reaches 4" W.G.
 - 9. Temperature of the system must be controlled to remain below the maximum temperature capability of the filter bags.
 - 10. The collector is now ready for use.

USING YOUR COLLECTOR

- ups (exception: after new bags are installed follow the INITIAL SYSTEM START UP procedure) should begin with all systems off. Turn on in the following sequence:
- 1. Filter bags installed, all ports, access doors and rotating equipment closed with safety equipment, (belt guards, etc.) in place.
- 2. Turn on compressed air.
- 3. After pressure reaches 185 psig minimum, turn on timer.

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- 4. Turn on all dust discharge equipment.
- 5. Turn on main fan@Preheat: system if necessary.
- You have purchased equipment to filter 1.9% of dust particles. If the collector urscharge is visible refer to the TROUBLE SHOOTING CHECK LIST that follows.

SHUTTING DOWN YOUR COLLECTOR

DUST CONTROL AND PNEUMATIC CON-VEYING SYSTEMS Reverse start-up procedure. First turn off the fan, wait five to ten minutes and turn off the timer and discharge (auxiliary) equipment.

PROCESS SYSTEM in Dryers hand the system to the collector discharge should be run until empty and heat maintained at a reduced rate until the collector metal surfaces and filter bags are dry. Then proceed as above. The system is the collector metal and the collector metal surfaces and filter bags are dry. Then proceed as above. The collector metal and the collector metals are surfaced as above.

ROUTINE MAINTENANCE

<u>SPECTION</u> Frequency will: vary as idely as there are operating conditions. Your experience will be the best guide. In general proceed as follows:

- 1. Daily adjust timer "OFF" time to achieve differential pressure of 4" W.G.
- 2. Weekly check timer and solenoid valves for proper operation. Usually listening to determine that there is an uniform time interval between solenoid air discharge blasts will suffice.
- 3. Monthly lubricate fan, rotary valve and screw conveyor. Inspect seals on latter two for dust loss.
- 4. Quarterly inspect filter bags for condition and that every bag clamp is *tight*.
- 5. Inspect, clean and replace air supply and differential filters as operating conditions require.

SAFETY Before entering dust collector:

- 1. Run cleaning mechanism 20 minutes with fan off to clean the filter bags.
- 2. Run solids out of the hopper.
- 3. Lock out electrical power on all rotating equipment.
- 4. If toxic gases and/or solids are present purge collector housing and block off inlet duct.
- 5. Install catwalks and safety cables.
- 6. Secure access doors in open position or remove doors by lifting from the hinge pins.
- ¹7. Use buddy system.
- 8. Wear respirator.
- 9. Use common sense.

TROUBLE SHOOTING CHECK LIST

First be sure that you have used the complete STANDARD START UP procedure.

PROBLEMS & PROBABLE CAUSES (SOLUTIONS) PROBABLE CAUSES VISIBLE EXHAUST DUST LOSS

- 1. Missing bag, dust loss will be constant not in synchronization with valve blasts. (Locate and replace missing bags.)
- 2. Improperly installed bags. Loose clamps or bag tops not clamped between cages and venturi collars. Constant dust loss. (Reinstall bags and cages properly.)
- 3. Holes in bags from mechanical damage during installation, abrasion, thermal or corrosive attack or wear. Generally in synchronization with valve blasts. (Replace worn or damaged bags with bags made from filter medium suitable for application. Plugging venturis with 3" diameter rubber plugs from the clean air (plenum) side of the collector is a quick temporary measure until the bags can be replaced.)
- 4. Dust in plenum after bags fail. (Always clean plenum before installing new bags.)

INSUFFICIENT AIR PRESSURE

- 5. Piping leaks. (Tighten fittings.)
- 6. Additional usage from plant system. (Revise system to furnish adequate air supply.)

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ENTIRE ROW OF BAGS INADEQUATELY CLEANED

- 7. Debris in diaphragm valve.
- 8. Dirt in solenoid plunger. (Remove solenoid cover and clean.)
 - 9. Solenoid valve inoperative. Electric, solenoid, or timer fault. (Establish power to solenoid and proper wiring to timer. Check solenoid and if O.K. change wiring at timer to next unused terminal and move

program wire to highest numbered terminal used or replace timer. If solenoid defective, replace.)

RANDOM BAG INADEQUATELY CLEANED

10. Debris in air distribution pipe hole. (Remove debris.)

HIGH DIFFERENTIAL PRESSURE

- 11. Excessive air flow. (Adjust fan damper until pressure gauge indicates proper pressure.)
- 12. Compressed air pressure below 75 psig. (See paragraphs 5 & 6.)
- 13. Solenoids skipping. (See paragraph 9.)
- 14. Reverse leakage through rotary valve. (Check rotary valve for wear or damage and correct.)
- 15. Dust on inside of bags after previous bag failure. (Clean plenum and inside of bags.) (See paragraph 4.)
- 16. Blinding (plugging) of bags due to condensables. (Change operations upstream so that liquids remain vaporized through unit. May be necessary to insulate the collector. Usually operating the collector with no solids flowing through will permit recovery.)
- 17. Re-entrainment of dust due to hopper overloading, bridging, or plugging. (Run out dust from discharge system with main fan off, consider increasing capacity of discharge system or reducing load and consider installing hopper vibrators.
- .18. Improper timer sequence. (Inspect timer for proper solenoid wiring and program wire position.)
- 19. Defective timer. (Return timer to us for repair or replace.)
- 20. Bags too tight. (If bags were cleaned they may have shrunk and are too tight to permit proper flexing. Replace bags.)

IMPROPER PULSING

- 21. Solenoid valves and working. (See
- Continuous air flow through diaphragm valve. (See paragraphs 7 & 8. Leak in tubing between solenoid and diaphragm valves.)

INSUFFICIENT DUST COLLECTION (SYSTEM VOLUME TOO LOW)

- 23. Fan running backwards. (Correct fan rotation.)
- 24. High differential pressure. (See paragraphs 5 through 9, 16, 17, 18 & 19.)
- 25. Fan belt slippage. (Tighten or replace belts.)

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- 26. Air short-circuiting between collection point(s) and fan. (Stop leaks.)
- Additions to system. (Increase system acity.)
- 28. System blockage. (Use proper shutdown procedure. Inspect piping for foreign material and remove. See paragraphs 9 and 15 through 19. Bags should feel soft to the hand or be replaced.)

SHORT BAG LIFE

- 29. High temperature. (Bleed in ambient air and/or replace with bags of high temperature rated fabric.)
- 30. Chemical attack. (Contact us for recommendation.)
- 31. Localized wear from rubbing. (Straighten cages so that bags do not rub against each other or the collector housing. Replace bags and corroded or broken cages. Wear at air inlet may require an inlet baffle.)

TIMER MALFUNCTION

- 32. "Power on" indicator light not on. (Ascertain that timer "ON-OFF" switch is on, that timer wiring is connected, and that indicator bulb is good. Inspect for blown fuse. Replace with 3 amp., 3 AG fuse. Do not use slow blow type.)
 - 33. Solenoids skipping. (See paragraph 9.)

UNUSUAL DIFFERENTIAL PRESSURE GAUGE READINGS

34. Unusual readings. (Inspect gauge filter, replace if plugged.) Blocked gauge tubing. (Disconnect and remove blockage. If blockage occurs frequently, install filter and replace it routinely.)

REPLACEMENT PARTS

Your ULTRA and FABRI-JET™ collectors use the finest components available. To ensure continued trouble free operation of your collector we recommend that only factory engineered components be used. The following components are suggested to be kept on hand to maintain trouble free service.

- 1. A spare set of filter bags and bag clamps.
- 2. Extra solenoid valves and diaphragm valves.
- 3. A spare timer board for multi-collector installations.

Our collector components can be used to maintain peak performance of collectors manufactured by Mikro Pul, Flex-Kleen and other leading manufacturers.

Operation and Maintenance Manual for Dry Electrostatic Precipitator Operations and Maintenance
Manual for
Dry Electrostatic Precipitator

1

BEFORE YOU BEGIN

1.1 ABOUT THIS MANUAL

Overview

This manual describes the basic operation and maintenance of the ENELCO® Electrostatic Precipitator. For information not included in this manual, contact the Environmental Elements Corporation, Field Engineering/Service Department.

Note: This manual does not attempt to cover all details of maintenance and operation. We recommend that the operator insert additional information based on experience.

If You Are a New User

The Environmental Elements Electrostatic Precipitator separates and collects suspended solids or liquids from gases. The equipment has been designed and constructed for simplicity and safety of operation, with a minimum of maintenance. At the same time, however, the principles of electrostatic precipitation are very different from those governing other types of electrical equipment. For this reason, it is important for you to be familiar with the procedures described in this manual.

What Does This Manual Include?

This manual includes the following sections:

SECTION	DESCRIPTION
Before You	General description of the manual and its
Begin	contents
Safety	Vital safety precautions for avoiding hazards
Precautions	associated with precipitators
Principles of	General overview of the precipitation process
Precipitation	•
Equipment	Functional descriptions of:
	internal components of the precipitator
1	electrical control and instrumentation
Starting Up the	Procedures for activating the precipitator
Precipitator	
Operating the	Procedures for:
Precipitator	operating the control console
_	operating the precipitator
Shutting Down	Procedures for shutdown preparations, and for
the	shutting down for brief or extended periods
Precipitator	

(continued)

2

SAFETY PRECAUTIONS

2.1 GENERAL PRECAUTIONS

Common Hazards

Electrostatic precipitators (ESPs) can pose the following hazards to personnel performing inspection, maintenance or repairs.

- electrical shock
- fire or explosion
- oxygen deficiency
- toxic chemicals and gases
- hot dust
- hopper-related hazards

These hazards, and the precautions to be taken against them, are described in greater detail in the following pages.

General Precautions

Before attempting to open or enter the precipitator, you must observe the following precautions:

- Shut down the precipitator, using the key interlock system
- · Ground the transformer-rectifier with safety ground devices
- Verify that no dust has accumulated behind the dry bottom doors
- Verify that no harmful gas is present in the precipitator
- · Shut down the ash removal equipment

2.2 PREVENTING ELECTRICAL SHOCK

Using the Key Interlock System

An electrostatic precipitator uses extremely dangerous high voltage! While the key interlock system prevents contact with energized parts of the high voltage system, this feature does not replace established safety measures. YOU MUST USE THE KEY INTERLOCK SYSTEM TO SHUT DOWN THE PRECIPITATOR. Use the following procedure.

Step	Action
1	Turn the OFF/RESET/ON switch (S1) in the control console to "Off". This deenergizes the associated transformer-rectifier (T/R) and frees an interlock key, which is then used to ground the T/R set. This must be done for each T/R set. Note The Key Interlock System schematic (Drawing D-810, located in Vol 3, Section 2) details the key interlock system and grounding procedure.
2	Manually ground all high voltage components of the precipitator before making any attempt to enter the precipitator, the insulator compartments or bus ducts. Safety grounding devices are provided for this purpose.

Using the Safety Grounding Devices

Use the following procedure to attach the grounding devices to the precipitator discharge electrodes in the insulator compartment (penthouse).

Step	Action
1	Clamp one end of the safety grounding device to a metal part of the precipitator structure that is connected to the station ground.
2	Attach free end of cable to the high voltage system member nearest the point
	of access. Continue, using other cables until all bus sections are grounded.

Before Welding Rigitrodes™

Observe the following precautions before performing any welding on the Rigitrode™ system.

- · Verify that all bus bars are disconnected at the insulator top plates
- Provide a visible ground wire from the insulator top plate to ground.

2.3 PREVENTING FIRE OR EXPLOSION

Warning

Fires can occur in any precipitator and ductwork during startup, operation, or shutdown!

Potential Causes

The following table lists possible causes of fire and explosion, along with methods for prevention.

Cause	Prevention
Fuel feed problem or turbine trip	Monitor boiler operation closely.
in boiler	Use established plant procedures to prevent boiler
	upset or trip conditions.
Unstable operation during startup	Observe safe startup procedures (see Chapter 5,
	Starting Up the Precipitator).
	Attend to all high level alarms immediately.
Improper purging during	Observe safe shutdown procedures (see Chapter 7,
shutdown	Shutting Down the Precipitator).
Flammable gas contacting a	Control combustible and oxygen levels by purging
source of ignition (e.g.,	completely and ventilating thoroughly before
cigarettes, matches, welding,	allowing personnel to enter the precipitator.
cutting torches, static electricity,	Keep work area well ventilated during service.
etc.)	Establish a monitoring program to guard against
	pockets of flammable gas.

In Case of Hopper Fire

If a fire or explosion occurs, the precipitator should be shut down to contain the damage. Fires should be allowed to burn out. If the fire is in the hopper, however, the fly ash should be removed via the ash conveying system.

2.4 HAZARD: OXYGEN DEFICIENCY

Causes of Oxygen Deficiency

In entering a confined space, flue gas will displace the existing atmosphere and reduce the oxygen content below the normal level of 20.8%. Combustible gases from collected particulate (e.g., methane, H₂S, etc.) can create pockets with reduced oxygen levels. Purging the unit during cooling does not always replace the flue gases with ambient air, and local gas pockets may remain.

Effects of Oxygen Deficiency

Oxygen levels below 20.8% result in rapid disability and death. Because the effects of oxygen deprivation are subtle, the victim commonly fails to recognize the symptoms, ignoring the danger until unable to escape from the hazardous environment.

Common symptoms of oxygen deprivation are a rapid pulse and increased rate of respiration, leading to loss of consciousness, irregular heartbeat, and muscular twitching. Unconsciousness and death can be sudden.

2.5 HAZARD: TOXIC CHEMICALS AND GASES

Typical Compounds

Any of the following chemicals and compounds may be found within a precipitator, depending upon its application:

CO

 H_2S

Total Reduced Sulfur (TRS)

Arsenic Lead

Cadmium Alkali Beryllium Acids

Zinc

Organic Solvents

 SO_2

 SO_3

Identifying the Risks

At the time of startup, a detailed analysis should be performed to determine the precise contaminants normally present in the precipitator.

Before personnel are permitted to enter, the air within the precipitator should be analyzed by a qualified safety officer with properly calibrated and maintained equipment.

Note Because oxygen and gas levels may change over time, this analysis should be repeated periodically while personnel are within the precipitator.

Training Personnel in Risk Management

A comprehensive risk management policy should be established and taught to all employees concerned with the operation, maintenance or repair of the precipitator. This policy should include the following:

- potential chemical hazards
- use of protective gear
- symptoms of exposure
- procedures for rescuing a victim of exposure

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Monitoring Gases Within the Precipitator

The EPA recommends the following procedures for testing gases within the precipitator.

Preparing to Sample Gases

Step	Action
1	Shut down the precipitator, using the procedure described in Chapter 7, Shutting Down the Precipitator.
2	Empty, purge, clean, and ventilate the precipitator as much as possible.
3	Open all access doors.
4	Lock out all electrical and mechanical equipment.
5	Isolate the dust collection area by closing dampers.

Sampling the Gases

Step	Action
1	Sample the precipitator gases at each of the access doors.
2	While remaining outside, use probes to sample gases inside the precipitator.
	Note Because many meters require oxygen near ambient levels in order to function, it is vital that the area be vented as thoroughly as possible before sampling.
3	Using probes, take samples in enclosed areas where pockets of gas would be likely to form.
4	If sufficient oxygen is present, the tester may enter the space and take samples from areas inaccessible from outside the shell. Pay particular attention to breathing zone areas. Note The tester must wear an air-supplied positive-pressure respirator while taking these samples.

Acting Upon Test Results

Depending upon the test results, the EPA recommends the following action:

- If flammable gases are still present, purge and ventilate the precipitator until the concentration is 10% of the lower explosive limit before personnel may enter.
- If the space contains insufficient oxygen, or toxic concentrations of other gases, all personnel entering the space must use an appropriate air-supplied respirator.

2.6 HAZARD: HOT DUST

Dangers of Hot Dust

Hot dust is very fluid, and it can quickly engulf and fatally burn a person. Dust temperature averages about 400°F.

Hopper Hazards

Because hot dust may accumulate behind the hopper access doors, these doors should be opened VERY CAREFULLY. Do not open the doors or enter the hopper until the precipitator has been shut down and the amount of accumulated dust, if any, is known. Unless maintenance or an inspection cannot be performed otherwise, the hopper doors should remain closed and locked at all times.

Checking for Accumulated Dust

After shutting down the precipitator, completely empty the hoppers, using the ash removal system. Before any personnel enter the hopper area, it is crucial that the following tests be completed satisfactorily.

Step	Action
1	Open the small port in each hopper door to see whether dust is trapped behind the door.
2	Strike the hopper door with a hammer. If the hopper is empty, you will hear a resounding ring. If it is full, the ash on the surface will muffle the blow, producing a dull thud.
3	To verify that no dust has lodged in the doorways, the corners, or the valleys of the pyramidal hoppers, perform an internal inspection from the top of the collecting surfaces, or from catwalks or lower-level access doors. Pay particular attention to the inlet and outlet plenums (nozzles), as these may accumulate enough dust to fill the hopper.

(continued)

2.6 HAZARD: HOT DUST

Final Test for Impounded Dust

The inner hopper door is fitted with U-shaped brackets, which capture the latch bar and provide the pressure to keep the door firmly against the shell. If all of the preceding tests have been completed satisfactorily, test for dust behind the door by using the following procedure.

Step	Action
1	To relax the pressure while the bar is inside the "U" shaped bracket, loosen the screw until the door can be moved away from the shell. Because the inner door may be dislodged and fall open, do not loosen the screw completely. Result: When the door moves away from the shell, if any dust is impounded behind the door, it will run out of the gap between the door and the shell. The door will still be kept in place by the latching bar.
2	When the pressure of the dust behind the door is eliminated, remove the latching bar and open the door. Have an escape path available if dust surges out.

If any dust has accumulated, it must be dislodged and removed before personnel enter the hopper. To do this, use any of the following methods while standing on the lower catwalk.

- washing with a high-pressure water hose
- poking

air lancing

- prodding
- mechanical vibration (via hammers or vibrators)

Do not attempt to remove the dust while inside the hopper. Falling dust can injure, suffocate or bury a person.

2.7 HOPPER-RELATED HAZARDS

Awkward Access

Due to the hopper angles, small door openings, and lack of internal handholds, personnel entering the hoppers can face a risk of falling. Proper temporary access equipment (e.g., scaffolds, ladders, handrails, etc.) should be installed according to OSHA regulations before maintenance personnel are allowed to enter.

Moving Dust

Do not operate the ash removal system (screws, drag chains, etc.) if personnel are inside or at risk of falling into the hoppers. When dust moves into the hopper, it becomes fluid and provides an unstable footing. Scaffolds on which workers may be standing can shift and float. Personnel can be engulfed in the moving dust.

2-10

PRINCIPLES OF PRECIPITATION

3.1 OVERVIEW

Elements of an Electrostatic Precipitator

An electrostatic precipitator consists of discharge electrodes of relatively small diameter (such as wire or the pins on a Rigitrode), positioned between collecting surfaces (plates or tubes). Between these collecting surfaces pass gases carrying entrained solid or liquid particles. Between the collecting surfaces and the electrodes is a unidirectional, high-potential field with rectified high voltage.

Charging the Particles

The discharge electrodes are of negative polarity, while the collecting surfaces are at ground potential and considered positive polarity. At and above a specific voltage, a corona discharge forms near the surface of the discharge electrode. This corona is a visible sign that positive and negative ions have been produced in the gas near the discharge electrode.

The positively and negatively charged gas ions are attracted to surfaces of opposite polarity. In moving toward these surfaces, the ions attach themselves to the solid or liquid particles entrained in the gas, in turn charging the particles either positive or negative.

Migration of the Charged Particles

The negative ions move toward the positive collecting surface, and the positive ions move toward the negative electrode. Because the ionization takes place near the discharge electrode, the negative ions have a greater distance to travel. Thus, more entrained particles are charged negative than positive. This results in a greater collection of particles on the grounded collecting surface than on the negative discharge electrode.

Discharging the Charged Particles

On reaching the collecting surface, the particles give up their charge and serve as a conductor for additional deposits of charged particles. Through cohesive, adhesive and electrostatic forces, a layer of collected particles is built up on the collecting surfaces.

Removing the Precipitated Particles

After a sufficient layer of particles has accumulated, they must be removed to maintain optimum operation. In a dry dust precipitator, rappers are used periodically to dislodge the ash buildup on the plates, causing the ash to fall into the hoppers. Dust removal equipment removes the ash from the hoppers. Hopper vibrators are run periodically to keep the ash fluidized for removal.

4

EQUIPMENT

4.1 PRECIPITATOR COMPONENTS

Areas of the Precipitator

The dry dust precipitator includes the following areas:

- Weather enclosure
- Penthouse
- Treatment zone
- Collection/disposal zone

Weather Enclosure

The weather enclosure is located on the precipitator roof, and contains the following components:

Component	Description
Transformer/ rectifier (T/R)	Supplies high voltage with unidirectional current to the discharge electrode system.
Automatic rapping system	Removes collected material from both the discharge electrodes and the collecting surfaces The EEC Field Engineer will perform initial adjustments of the rapping system at startup.
Fan(s)	Ventilates the weather enclosure to keep equipment cool.
Penthouse pressurization heating system	Prevents moisture from forming on the high voltage system insulators in the precipitator penthouse. Important: To maintain the insulators in good condition, penthouse heaters must be operating at the following times: • at least four hours before the precipitator is activated. • whenever gas is passing through the precipitator
Fan(s)	• during all but lengthy outages Provides positive pressurization to prevent flue gases from infiltrating the penthouse from the treatment zone.
Plate rappers	Trigger impact against the collecting plates to dislodge collected particulate.

(continued)

PRECIPITATOR COMPONENTS

(continued)

Penthouse

The penthouse is located between the precipitator roof and the treatment zone, and typically includes the following components:

Component	Description
High- voltage support system	Transports high voltage to the discharge electrodes suspended in the treatment zone.
Insulators	Isolate the high voltage system from the precipitator casing, which is at ground potential. Composed of alumina, the insulators are kept dry by the penthouse pressurization/heating system. Important: To prevent "arc-over", insulators must be kept free ofdust and moisture at all times.
Rapper spring plate assembly	Transfers high voltage to the electrode frame, and provides a means of rapping (cleaning) the electrode frames.

Precipitator Treatment Zone

The precipitator treatment zone is a box like enclosure, open to the ductwork on the ends. Gas enters at one end (inlet), is cleaned of suspended particles, and is discharged through the other end (outlet). The precipitator treatment zone contains the following components:

Component	Description
Collecting surfaces	A vertical arrangement of collecting surfaces forms multiple gas passages. Passages are parallel to the gas flow, and open to the ductwork at the precipitator inlet and outlet. Collecting surfaces are usually placed in series to form fields.

High-voltage discharge electrodes	Negatively charged electrodes are suspended between the collecting surfaces from high-voltage frames. These frames are suspended by the high-voltage support system. Below the gas passages, the discharge electrodes are guided by a rigid frame suspended from the electrodes. The discharge electrodes may be aligned in the passages, using adjustments built into the high voltage structure support system.
Plate rapper anvils and rapper rods	Transmit the force from the rappers to collecting plates, dislodging the fly ash.
Gas distribution devices	Located at the inlet and outlet of the precipitator chamber, gas distribution devices regulate the velocity in all gas passages.

(continued)

PRECIPITATOR COMPONENTS

(continued)

Collection/Disposal Area

Collected materials, dislodged from the discharge electrodes and collecting surfaces, fall through the gas passages into the hoppers below. The collected material is then removed from the hoppers by the dust removal system.

The collection/disposal area of a utility boiler precipitator includes the following components:

Component	Description
Hopper discharge	Provides collection point for customer- supplied ash removal equipment
flange	

4.2 ELECTRICAL CONTROL & INSTRUMENTATION

Control Console

The operating controls for the T/R unit are remotely located in a self-contained control console. The control console provides the following meters, which display the voltage at various points of the transformer-rectifier and precipitator.

Meter	Description	
Voltmeter (VM)	Indicates the AC RMS voltage on the primary circuit of the T/R.	
Ammeter (AM)	Reads the AC RMS current in the primary circuit of the T/R.	
Milliammeter	Indicates DC current flowing in the precipitator field. The milliammeter	
(MA)	is connected in the ground side of the rectifier.	
	Note: If there is an open circuit, the miliammeter is protected from	
	high voltage by surge arrestor(s) located in the T/R set low	
	voltage junction box.	
Kilovolt meter	Indicates the DC voltage on the discharge electrodes.	
(KV)	Note: If there is an open circuit, the kilovolt meter is protected from	
	high voltage by surge arrestor(s) located in the T/R set low	
	voltage junction box.	

ELECTRICAL CONTROL & INSTRUMENTATION

(continued)

Transformer-Rectifier Operating Controls

The table below lists the most vital T/R controls. For complete information, see technical manual ME-100.

Control	Description
Off/Reset-On Key Interlock (S1)	Also called the Control Console switch. Has two settings: Off/Reset and On. To turn off and/or reset the alarm circuit, set S1 to "Off/Reset" if contactor K1 opens due to any alarm or loss of line voltage Note: An alarm is not generated if the console is turned off by means of S1.
Secondary Voltage Limit Thumbwheels	Sets the maximum secondary voltage allowed before the Digicon Optipulse Control limits the T/R console in Automatic mode. The absolute high limit is factory set for the specific T/R size.
Integral Grounding Device	Air switch located above the tank. The external operating handle is key interlocked, prohibiting movement while energized. Before you can turn and lock the switch, you must deenergize the transformer-rectifier and transfer the operating key (KI) from the control console switch (Sl) to its alternate lock in the transformer-rectifier switch. The switch can only be locked in the ground position.

Internal Components of the T/R Control Console

The internal components of the transformer/rectifier control console are listed and described in detail in technical manual ME-100.

5
STARTING UP THE PRECIPITATOR

5.1 PRELIMINARY STARTUP PROCEDURES

Precautions to Take Before Starting Up

Take the following precautions before energizing the precipitator.

STEP	ACTION
1	Inspect the precipitator for tools or debris.
2	To check for unobserved grounds, disconnect the high voltage bus in the penthouse and measure the resistance of each field to ground, using a 1000-volt megger. The result should be between 100 mega-ohms and infinity. Note: Collecting electrodes and Rigitrodes TM must be centered between the collecting surfaces, no more than 3/4 inches off the center line.
3	Start the penthouse pressurization/heating system no less than 4 hours before you energize the precipitator.
4	Visually inspect each T/R set for signs of damage: • fluid leaks • bowed access covers or tank walls (indicating high internal pressure)
5	Verify that fluid level is within the acceptable range.
6	Close and lock the precipitator and insulator compartment doors, using the key interlock procedure described in Drawing D810, Section 2 of volume 3.

Systems to Start Up Before Energizing the Precipitator

The following systems must be operating when the precipitator is started up.

System .	Must be operating when
Collected material conveying system	gas is passing through precipitator
Discharge electrode and collecting surface rappers	when the precipitator is energized
Penthouse heating and pressurization system	four hours before precipitator is energized.
Floor heaters	four hours before gas begins passing through precipitator
Slide gates	(open) before starting I.D. fan

5.2 STARTUP PROCEDURES

Precautions to Take Before Energizing the Transformer-Rectifier

Do not allow the transformer-rectifier to become disconnected from the load while energized!

The rectifier switches are interlocked to prevent the T/R from becoming disconnected while the switches are being operated. Before moving the rectifier switch, verify that the control console circuit breaker is open and locked out.

Energizing and Regulating the Transformer-Rectifier

To energize the T/R and regulate it for proper operation, use the following procedure.

Step	Action
1	Turn the high voltage selector switch (located on or above the T/R) to the "HV" (full wave) position. Result The access key is held captive and the operating key is released, allowing power to be applied to the unit from the control console (for more information, see Drawing D810 in Section 2 of volume 3).
2	Verify that the auto-test switch (S2, located on the control console) is in the Automatic position and that the thumbwheel switches are properly set.
3	Turn switch Sl to the "On" position. (See the Drawing D810 for a detailed description of this sequence.)
4	Check the meters on the control consoles to verify that power is increasing to normal operating levels. Refer to the Troubleshooting section of technical manual ME-100 if any problems occur.

Note: Once adjusted at time of start up, the automatic voltage control should not require readjustment unless precipitator operating conditions change greatly. If, at any time, there is evidence that the automatic voltage control is not functioning properly, refer to technical manual ME-100: Digicon Optipulse Controller and Rectifier Control Console.

6

OPERATING THE PRECIPITATOR

6.1 OPERATING THE CONTROL CONSOLE

Introduction

You may operate the precipitator control console in either of the following modes:

· Test:

Sets up conditions for testing circuits and precipitator performance

· Automatic:

Sets up conditions for normal operation

For more information, see drawing D807, in Section 2 of volume 3.

How to Operate the Console in Test Mode

Caution:

Do not leave the consoles running in test mode. Some of the automatic control features are not active in the test mode; therefore, precipitator performance must be closely monitored by maintenance personnel.

Step	Action
1	To apply power to the control console, close the circuit breaker, which is
	located in the control console or in the motor control center.
	Result: The control console is energized, and the white light (WIL) lights.
2	To operate the control console under test mode, place the automatic/test
	selector switch (S2) in the test position.
	Note: Do not leave the precipitator unattended when it is operating in the
1	test mode!
3	Before closing the main contactor (K1), be sure that the test control
1	potentiometer (R8) is turned fully counter-clockwise.
4	Close contactor K1 by turning the selector switch (S1) to the "On"
	position.
	Result: The high-voltage T/R is energized, indicated by the red "High
	Voltage On" light (RIL).
5	Regulate precipitator voltage by slowly turning the test control
1	potentiometer (R8) clockwise.
	Note: In Test mode, all voltage and current trips are active. The DOC will
1	trip the T/R control console if the default sparkover rate of 240
	spm is exceeded.

OPERATING THE CONTROL CONSOLE

(continued)

How to Operate the Console in Automatic Mode

STEP	ACTION
1	To apply power to the control console, close the circuit breaker, which is
	located in the control console or in the motor control center.
	Result: The control console is energized, and the white light (WIL) lights.
2	To operate the control console under automatic mode, place the
_	automatic/test selector switch (S2) in the automatic position.
3	Close contactor K1 by turning the selector switch
	(S1) to the "ON" position.
	Result: The high-voltage T/R is energized, indicated by the red "High
	Voltage On" light (RIL).
4	Adjust the secondary voltage of the precipitator to the sparkover point, the
	T/R voltage limit, or the T/R current limit by turning the Secondary
	Voltage Limit Switch thumbwheels on the DOC.
5	The spark response switch regulates the controller reaction time to
	sparking. Refer to technical manual ME-100 for details. DO NOT
	CHANGE WITHOUT AUTHORIZATION FROM EEC.

Note: The location of the components, the wiring diagrams, and the electrical schematics can be found with the electrical drawings in the Appendix. For more detailed information on operating the console, see technical manual ME-100.

6.2 OPERATING THE PRECIPITATOR

Introduction

Because the precipitator's collecting efficiency increases as the applied voltage increases, voltage should be kept at a point that produces a light sparking condition or current limit. The Digicon Optipulse Controller automatically maintains the T/R's voltage output at this ideal level.

How Is the High Voltage Set Point Determined?

The ENELCO® Field Engineer determines the high voltage set point according to the existing conditions of gas loading (usually at rated gas volume). Normally, as the set point is at the upper limit, this operating value will be varied automatically as the gas load conditions vary. If the spark rate becomes excessive, however, this point can be lowered.

Note: If one or more conditions change significantly within the precipitator, the T/R control console will reflect the change.

How Do Varying Conditions Affect Precipitation?

The factors listed below illustrate common influences on the effectiveness of the precipitator.

Moisture

An increase in the moisture content of the gas will increase electrical conductivity. This causes a decrease in sparkover voltage and an increase in precipitating current. The presence of water vapor improves precipitation, and an inadequate amount is a restriction to good performance.

Dust Concentration

An increase in dust concentration is usually accompanied by a decrease in sparkover voltage and precipitating current. The increase in dust concentration can result in an increase in the amount of dust that is collected. However, as the dust concentration is increased, the amount of dust that is not collected will also increase. In addition, the discharge electrodes and collecting surfaces will demand more frequent rapping.

A decrease in dust concentration reverses these conditions: while the sparkover voltage and precipitating current are higher, less dust is collected and less dust is emitted.

OPERATING THE PRECIPITATOR

(continued)

Flow Rate

An increase in gas velocity will decrease the collecting efficiency and increase the amount of dust not collected. It is best to operate at or below the rating of the precipitator.

Cleanliness of Electrodes and Collecting Surfaces

Limiting the accumulation of dust on the discharge electrodes and collecting surfaces is essential to the efficiency of the precipitator. For the recommended rapping timing and pattern, see drawings A890 and A891.

Component	Effect of Dust Buildup
Discharge Electrodes	Reduces the corona discharge, thus reducing precipitating current.
Collecting Surfaces	Reduces clearance between electrode and collecting surface, thus lowering collecting efficiency. Reduces clearance between the discharge electrodes and the collecting surfaces, which can lower sparkover voltage. Increases re-entrainment of collected particulate matter, which decreases collecting efficiency.

7

SHUTTING DOWN THE PRECIPITATOR

7.1 EMERGENCY SHUTDOWN

Shutting Down in an Emergency

To shut down the transformer/rectifier completely, open the circuit breaker.

7.2 SHUTTING DOWN FOR AN EXTENDED PERIOD

Preliminary Procedure

Before shutting down the precipitator for an extended period, use the following procedure.

Step	Action	
1	Shut down boiler.	
2	Shut down I.D. fan.	
3	Close I.D. fan isolation gate, preventing particulate and gas from exiting the precipitator.	
4	Turn off all fields. Important: The outlet field should continue to operate at the lower kV setting only if the following conditions apply Opacity excursion is not allowed at shutdown Natural draft is allowed (i.e., the fan damper is open) If internal inspection or repair is being performed, the damper should remain open to allow air movement through the box.	
5	Rap down plates for at least four hours, using clean-down program # 2.	
6	After the rappers are turned off, the ash removal equipment should continued to operate for at least four hours.	
7	Continue with the following procedure: Before Opening the Penthouse.	

SHUTTING DOWN FOR AN EXTENDED PERIOD

(continued)

Before Opening the Penthouse

Step	Action
1	Perform preliminary procedures.
2	Turn off penthouse blower/heaters.
3	Turn off outlet field.
4	Follow T/R grounding procedure described on Drawing D810, Key
l	Interlock System (see Section 2 of this volume).
5	Open the following access doors:
	Weather enclosure
<u>l</u>	Precipitator floor
6	Allow the penthouse to cool to 100°F or below, according to your facility's
	confined space entry procedure.
7	Check for hazardous gases and verify that sufficient O2 is present in the
1	precipitator. Follow established plant procedures for entering confined
	space. See Chapter 2, Safety Procedures, for further information.

When Opening the Penthouse

Use the following procedure when opening the penthouse.

Step	Action
1	Enter according to established procedures for confined spaces.
2	-Ground all high-voltage bus bars with grounding devices provided.
3	With a portable sniffer available, open one hot roof door.
4	Look for glowing material on plates or on hopper floor. If any is present, SHUT DOOR IMMEDIATELY AND EXIT PENTHOUSE. Repeat steps 3 and 4 hourly until no glowing material is present.
5	Carefully open remaining doors, checking at each door for glowing material. If any material is present, SHUT ALL DOORS IMMEDIATELY AND EXIT THE PENTHOUSE.
6	After all doors are open, exit the penthouse.
7	Mark all open doors to prevent unauthorized entry.

SHUTTING DOWN FOR AN EXTENDED PERIOD

(continued)

Opening the Dry Bottom

Step	Action
1	Using the peepholes and other safety features, check for collected material
	lodged behind the doors.
$\frac{1}{2}$	If no dust is visible, open the door while leaving the interlock locked. This
	prevents the door from springing open, possibly exposing you to hot dust.
3	When dust has finished spilling out, close the door and unlock the interlock.
4	While leaving an escape path available, open the door away from you.
5	Attach ground cables to the Rigitrode™ frame.
6	Repeat steps 1-5 for all remaining doors.

Before Entering the Precipitator

Observe the following precautions before entering the precipitator box.

Action
Allow the box to cool with all doors open for 12-16 hours, or until the
internal temperature is below 100°F.
Follow established company procedures for working in enclosed space.
Ensure that a qualified safety officer is present at all times when personnel are inside the precipitator.

7.3 SHUTTING DOWN FOR A BRIEF PERIOD

Preliminary Procedure

Before shutting down the precipitator for a brief period (less than 48 hours), use the following procedure.

Step	Action
1	Shut down boiler.
2	Close I.D. fan isolation gate.
3	Turn off all fields, except outlet field.
4	Rap down plates for at least four hours, using clean-down program # 2.
5	After the rappers are turned off, the ash removal equipment should continue to operate for at least two hours.
6	Continue with the following procedure: Before Opening the Penthouse.

Before Opening the Penthouse

Before opening the penthouse or allowing personnel to enter, perform the following procedure.

Step	Action
1	Turn off the penthouse heaters. To allow the area to cool, keep the blower
	operating.
2	Follow the key interlock procedure for grounding the T/R.
3	Open the access doors in the weather enclosure floor (or penthouse roof)

8

MAINTAINING THE PRECIPITATOR

8.1 PRELIMINARY MAINTENANCE

Recording Normal Meter Readings

On a daily basis, monitor the readings of the metering system in the precipitator control room. Establish a normal range for these meters; this will enable you to note any radical changes.

Preparing Plan View Maps

Before performing regular inspections, prepare a plan view map of each field showing plates, electrodes and rapper rods. This will assist you in inspecting the upper and lower portions of the precipitator treatment area.

For Additional Information

Further requirements and procedures for maintenance and inspection are listed in the auxiliary manuals for precipitator components. Before performing maintenance or inspection, personnel should be familiar with all available procedures.

8.2 DAILY INSPECTION PROCEDURES

Purpose

This section is intended to be used as a guideline rather than as an exact listing of all possible points for inspection. The inspectors at your facility are encouraged to develop their own supplementary list.

Daily Inspection

The following items should be inspected on a daily basis.

Step	Action
1	Visually verify that all rappers are operating properly.
2	Check all T/R oil temperatures.
	Note the highest temperature recorded by the red "memory" needle.
3	Listen for sounds of arcing in and around the T/R sets.
4	Record a complete set of T/R readings under a known set of boiler operating conditions. Compare these readings with the desired readings. Note The following readings indicate trouble and should be investigated: low voltage and high current normal voltage and low current
5	Verify that the automatic T/R controllers (DOCs) are functioning properly.
. 6	Observe readings given by the metering system in the control room. Note any radical variations from the normal pattern (see <i>Preliminary Maintenance</i>).
7	Verify that the stack opacity monitor is functioning properly.
8	Verify that all blowers are operating properly. Check penthouse blower filters and replace (if necessary).
9	Verify that the penthouse pressurization/heating system is operating properly.
10	Check for any new casing gas leaks or worsening of known leaks.
11	Check for any liquid leaks.
12	Check all expansion joints during a routine walk-down. Observe signs of leakage and ensure that leaks are repaired at the earliest opportunity.
13	Verify that the dust removal equipment is functioning properly.

8.3 WEEKLY INSPECTION PROCEDURES

Purpose

This section is intended to be used as a guideline rather than as an exact listing of all possible points for inspection. The inspectors at your facility are encouraged to develop their own supplementary list.

Weekly Inspections

The following procedures should be performed weekly, or according to the facility's precipitator maintenance program.

Step	Action
1	Check all motor bearings for high temperature and signs of excessive vibration.
2	Verify that all blower filters are clean. Replace dirty filters when necessary. Maintain a record of filter changes to diagnose possible problems. Note While this procedure should be performed weekly immediately after initial startup, the intervals may be lengthened as the precipitator continues to operate

8.4 MONTHLY INSPECTION PROCEDURES

Purpose

This section is intended to be used as a guideline rather than as an exact listing of all possible points for inspection. The inspectors at your facility are encouraged to develop their own supplementary list.

Monthly Inspections

The following items should be inspected on a monthly basis.

Step	Action
1	Check all drive belts for tightness and general condition.
2	Check the overall condition of individual rappers, including (but not limited to) ground straps, boots, and rapper body.
3	Check for loose nuts or broken track welds on rapper all-thread rods.
4	Visually inspect the general condition of all T/Rs.
5	Inspect the outer access doors and gaskets. Note any signs of leakage. Repair leaks at the earliest opportunity.

8.5 SEMI-ANNUAL INSPECTION PROCEDURES

Purpose

This section is intended to be used as a guideline rather than as an exact listing of all possible points for inspection. The inspectors at your facility are encouraged to develop their own supplementary list.

Weather Enclosure (or Roof)

Step	Action
1	Verify that all rapper boot clamps are in place.
2	Verify that seals are tight on all cold roof doors.
3	Check bus bar path and connections for dirt and close clearances.

Penthouse Area

Step	Action
1	Check for evidence of tracking or cracks in high voltage support insulators.
2	Verify that venturi holes are clear on high-voltage support insulator top plate
3	Verify that the 2" nut retainer (keeper angle) on the high voltage frame support rod is in position.
4	Check for signs of tracking on or warping of the melamine rapper rods. Wipe down where necessary.
5	Check rapper tube purge holes for plugging or corrosion. Ensure that holes are open to allow purge air flow.
6	Check for accumulation of dust in penthouse. Vacuum clean if necessary. Determine the cause of excessive accumulations and take corrective action.
7	Check ceiling insulation or floor block insulation for damage or uncovered areas. Repair uncovered areas as required.
8	Check the bus bar jumper connections and welds to the top plate of the high voltage support insulator.
9	(If applicable) Verify that insulator band heaters are tight around perimeter of the high voltage insulator. Test heaters for proper ohmic value.
10	(If applicable) Check thermal tape around joints of the casing heat piping.
11	Look for signs of wall buckling, condensation, air inleakage, or corrosion.
12	Check melamine rods for tightness in lower sockets.
13	Check the integrity of the expansion joints in the heater purge air system.

SEMI-ANNUAL INSPECTION PROCEDURES

(continued)

Inside Upper Treatment Area

Step	Action
1	Check for excessive bridging or buildups that might cause grounding or close
	clearances.
	Note Perform this check before cleaning the precipitator.
2	Check inside bell housing for tracking or buildups.
3	Verify that the nozzles are pointed in the proper direction.
4	Clean between plate support channel and wall, and support beams.
5	Measure distance from the bottom of the bell house to the hanger rod,
	ensuring that at least the minimum clearance recommended by the
	manufacturer is maintained.
6	Check for loose Rigitrodes™ and tighten where necessary.
7	Check mine bolts for wear where the mine bolt passes through the upper toe
1	of the place support channel.
8	Verify that the channel spacer bar is loose but secure.
9	Verify that the four studs are present on the rapper anvils and that the rapper
	rods are between the studs.

Inside Lower Treatment Area

Step	Action
1	Check for loose Rigitrodes™.
2	Verify that perforated plate rapper is intact.
3	Check perforated plates for binding on sides or bottom.
4	Check inlet/outlet plenum perforated plates for pluggage and buildups.
5	Check for excessively loose plate tadpole pins and worn guide strips.
6	At several points, observe and map clearance between walls and baffles to the plate and electrode frames.
7	Inspect access doors and gaskets for tight seals or corrosion.
8	Check the condition of the Teflon™ anti-sway bars. Verify that the Teflon™ is clean and flexible.

SEMI-ANNUAL INSPECTION PROCEDURES

(continued)

Collection/Disposal Zone

Step	Action
1	Inspect the access doors and gaskets for tight seals or corrosion.
2	Inspect the screw conveyor (if supplied) for bent flights.
3	Inspect hopper walls for warping or evidence of corrosion.
4	Check for pluggage in the ash removal system.

Cleaning the Precipitator

The following areas should be cleaned with a dry clean cloth or electric cleaner at least twice a year.

- all standoff insulators
- outside surfaces of the high-voltage support insulators
- inside surfaces of high voltage insulators

8.6 ANNUAL INSPECTION PROCEDURES

Purpose

This section is intended to be used as a guideline rather than as an exact listing of all possible points for inspection. The inspectors at your facility are encouraged to develop their own supplementary list.

Weather Enclosure (or Roof)

Step	Action
1	Verify that rapper rods are free in their exit bushings.
2	Verify that the air switch is functioning properly.
3	Verify that the T/R switch blade is in good condition.
4	Check the T/R oil level. Add oil if necessary.
5	Run carbon and dielectric tests on T/R oil.
6	Check the operation of the key interlock system; lubricate locks with dry
	graphite. Do not use oil lubricant with the key interlock system.

Inside Upper Treatment Area

Step	Action	
1	Check for separation of tadpole pins from the plate's top edge.	
2	By shining a flashlight down the length of the plate, check for:	
	bowing plates or Rigitrodes™	
	• bent pins	
	 possible close clearances 	
	general alignments	
	Note any significant differences in the field maps.	

ANNUAL INSPECTION PROCEDURES

(continued)

Inside Lower Treatment Area

Step	Action	
1	Take random pin-to-baffle and pin-to-plate measurements.	
2	Check above baffle between fields for buildups.	
3	Check for bowed plates by measuring from plate to plate.	
4	Look for corrosion on collecting plates, possible thinning of plates, or holes in plates	
5	Check for signs of excessive heat.	
6	Verify that the "J" hooks holding the perforated plates in position are fixed to the casing wall.	

Collection/Disposal Zone

Step	Action
1	Check tightness and condition of bearings and couplings.

Rapper Controls

To establish a base line for future inspection and analysis, a reference sheet should be created, containing the desired settings for the rapper system.

Step	Action
1	€onfirm the system timing sequence for each field from the reference sheet.
2	Confirm the impact rapper lift from the reference sheet.

Outside the Precipitator Shell

Step	Action	
1	Check the external condition of insulation and lagging for any missing pieces	
<u></u>	or areas in need of repair.	

8.7 BIENNIAL INSPECTION PROCEDURES

Purpose

This section is intended to be used as a guideline rather than as an exact listing of all possible points for inspection. The inspectors at your facility are encouraged to develop their own supplementary list.

Precipitator

The following areas should be inspected at least once every two years.

Step	Action
1	Verify balanced draw and correct current level on all phases of all motors and heaters.
2	Check piston exposure on all rappers, and verify that all rapper bodies are true to plumb.
3	Measure field clearances to determine whether realignment is required.
4	Check inside the T/R controllers and rapper panel for dust buildup.
5	Megger T/Rs and compare recorded readings against equipment baseline data.
6	Check hopper corners for buildups and corrosion.
7	Megger hopper heaters, replace if necessary.

High Voltage Controllers

Step	• Action	
1	Check accuracy of all control console meters.	
2	Calibrate primary current overload relay.	
3	Fest all alarm and trip functions by simulation.	
4	Torque check all wiring connections on both high-voltage and low-voltage systems.	
5	Inspect the precipitator ground grid and ground connections. Inspect connections to T/Rs, control consoles and structure to earth.	

8.8 TRIENNIAL INSPECTION PROCEDURES

Purpose

This section is intended to be used as a guideline rather than as an exact listing of all possible points for inspection. The inspectors at your facility are encouraged to develop their own supplementary list.

Areas for Triennial Inspection

The following areas should be inspected at least every three years.

Step	Action
1	Check plate thickness to determine the degree of corrosion.
2	Check duct work approaching and exiting the precipitator for areas of
	buildup or failed turning vanes.

9
TROUBLESHOOTING GUIDE

9.1 GENERAL TROUBLESHOOTING PROCEDURES

Common Problems

The following table lists common problems that occur in precipitators, along with ways to prevent or correct them.

Component	Possible Problem	Prevention/Correction
Insulators	Dust buildup	Open insulator compartments and clean
		surfaces. Do not apply polish. Such
		substances may trigger electric flashover,
		causing insulator failure.
	Cracks	Replace, using new gaskets.
	Carbon tracking	Realign high voltage frames (if needed)
T/R Unit	Inadequate ventilation (due	T/R units are self-cooled and depend
	to high ambient	entirely upon surrounding air for dispersing
	temperature trip)	heat. Ensure adequate ventilation and
		airflow around tank.
		Note A temperature indicator is provided.
T/R Tank	Poor fluid quality	The T/R units are shipped filled with
		transformer fluid. Samples of the fluid from
		T/R tank should be tested for conductivity
]	at least once every six months. Keep
· ·		records of test results.
	Insufficient fluid (due to	Check the fluid level regularly. If the tank
	high T/R temperature)	needs to be refilled with fluid, use only type
		specified on nameplate.
		Note: A sight glass is provided.
Control Console	Dust buildup	Vacuum internal parts occasionally.
		Warning: Do not disturb wiring or
		connections.
	Loose connection(s)	Tighten the connection(s).
	Evidence of burning	Check for loose connection; tighten or
		replace wiring. DO NOT SPLICE.
	High ambient temperature	Verify that fans are working correctly.
	trip	Check filters (if supplied). Replace if
		necessary.

GENERAL TROUBLESHOOTING PROCEDURES

Common Problems (continued)

Сотролепt	Possible Problem	Prevention/Correction
Collecting	Excessive dust buildup	Clean before re-
surfaces	(> ¹ / ₄ ")	energizing. Adjust
		rapping frequency.
Discharge	Dust buildup	Clean before re-
electrodes	_	energizing.
		Adjust rapping
		frequency.
	Unequal clearance	Each electrode must be
1	between electrodes and	spaced no more than
	collecting surfaces	3/4" off the
	-	centerline between the
		collecting surfaces.
Interlocks	Difficult to operate	Apply powdered
	_	graphite to a key.
		Insert and turn the
		key in the lock. DO
		NOT USE OIL.
	Damaged chains	Repair chains.
Perforated	Plugged with dust	Clean.
plates	deposits	İ
Penthouse	Dust in penthouse area	Clean/change filters
pressurizat		often. Verify that
ion/		fans are operating
heating		properly. Check
system	• •	precipitator roof
)		doors for proper fit
		and seal.
•	Low penthouse	Check heater
	temperature	operation. Verify that
		the thermocouple and
1		thermostat are
		operating properly.
High	Dust buildup	Open insulator
voltage		compartments and clean
support		surfaces.
insulators		
¥	Cracks	Replace, using new
1		gaskets. Realign high
		voltage frames
	Carbon tracking	(if necessary).

GENERAL TROUBLESHOOTING PROCEDURES

Common Problems (continued)

Component	Possible Problems	Prevention/Correction
Rappers	Piston is not lifting Piston is hitting top of rapper	Perform diagnostic inspection: • Verify that rapper panel is ON • Check rapper panel for loose wires. • Check rapper coil and DC output card for short circuit(s) • Check rapper for magnetic charge Report findings to EEC Field Service. Perform diagnostic inspection: • Check number of pulses indicated
		 in the rapper panel program Check the exposure of the rapper piston. Report findings to EEC Field Service.
Door gaskets	Deterioration or in-leakage	Replace as necessary
Ductwork	Deterioration Leaks	Call Environmental Elements Corporation Tighten bolts
		Call Environmental
Structural joints	Leaks or general deterioration	Elements Corporation

9.2 DIAGNOSING AND SOLVING SPECIFIC PROBLEMS

High Spark Rates

It is normal in most applications for the inlet fields of the precipitator to spark. An excessively high spark rate that inhibits the power input of any field, however, may indicate a problem. Some of the more likely causes follow.

Possible Cause	Action
High dust concentration in flue gas	Check boiler operation
	Check operation of any pre-collectors
High gas velocity through the	Check boiler operation
precipitator	Check gas distribution devices for blockages or
	damage
Dust build-ups within	Check rappers
the precipitator	Check dust conveying system
Close or unequal clearances within the	Inspect and correct clearances
precipitator	
T/R failure	Follow megger instructions to determine the T/R
	condition; contact Environmental Elements
	Corporation Field Service.
Insulator failure	Verify that penthouse heating system is working
	and is being activated four hours before the
	precipitator is started up.
	Inspect high voltage support insulators, high
	voltage rapper rods, and all other HV distribution
	stand-off insulators. Replace any insulators that
	are cracked or show signs of electrical tracking.
Grounded field	Perform an internal inspection to determine the
	cause of the ground.
High air flow	Check boiler operation.
High moisture content in flue gas	Check boiler operation.

DIAGNOSING AND SOLVING SPECIFIC PROBLEMS

(continued)

Abnormal Power Readings

Many precipitator problems may be indicated and possibly diagnosed by using the T/R voltage and current meters. Some of the more obvious indications follow.

Meter Indications	Probable Cause(s)	Action(s)
Zero voltage, all other indicators normal	Bad voltmeter	Repair/replace
	Grounded field	Inspect, remove ground
	Failed T/R	Megger T/R to confirm; call EEC Field Service
Zero voltage, excessively high current, and shutoff on overcurrent	Overloaded conveying system	Check dust level and remove excessive amounts
	Grounded high voltage component	Inspect, remove ground
	Failed T/R	Megger T/R to confirm, contact EEC Field Service
Voltages slowly decrease as current increases, and	Dust bridges within the	Check rappers
	precipitator	Check dust conveying system
shut off on under-voltage	Overloaded conveying system	Check dust level and remove excessive amounts
Milliameter reads zero; all	Bad milliameter	Repair/replace
other meters show normal readings	T/R failure	Megger T/R to confirm, contact EEC Field Service
Field operates at kV limit	Faulty kV metering circuit	Replace the failed resistor(s)
of T/R rating; all other	resistors	
meters read zero or very low	Possible open-circuited metering resistor in T/R low voltage junction box	

DIAGNOSING AND SOLVING SPECIFIC PROBLEMS

(continued)

Increased Opacity

All the problems mentioned above can result in higher opacity levels (increased dust emission). Other items that could cause an increase in opacity follow.

Possible Cause	Action
Improper rapper cycle times and/or	Readjust rapper times and/or intensity
intensity	according to Drawings A890 and A891.
Improper gas flow distribution,	Check distribution media for damage or
causing high gas velocity in areas of	blockage
the precipitator, and reducing the	
treatment time	
Precipitator is full of dust, causing re-	Remove dust and verify that removal system is
entrainment of collected dust	working properly
Flue gas leakage around the treatment	Check baffling for damage
zone (above, below, or along the	
sides)	
Gas volume above the rated design,	Conduct pitot tube traverse to determine gas
causing increased velocity within the	volume
precipitator and reducing treatment	
time	
Improperly adjusted controls	See technical manual ME-100 to correct
	control problems
Change in dust particle size	Verify boiler operation. Verify that coal
4	supplier has not changed.

Additional Resources

For additional information, refer to the following resources:

Resource	Information Provided	
Appendix	Mechanical and electrical schematic drawings and diagrams	
Technical Manual ME-100	Installation, operation, maintenance, and troubleshooting details of the Digicon Optipulse Controller and Rectifier Control Console	
Auxiliary Manuals	Installation, operation, maintenance and troubleshooting details of precipitator components manufactured by contracted vendors	

Operation and Maintenance Manual for Venturi Scrubber

501.000 Subcooler Venturi Scrubber

501.000 Subcooler	Venturi Scrubber
	on & Maintenance Manual
	n 1: Hydromist Venturipak Wet Scrubber Introduction
	n 2: Sub-Cooler Impingement Tray Stage
501.001.3 Section	n 3: Condenser Mist Eliminator Stage
501.001.4 Sectio	n 4: Venturi Impingement Tray Stage
501.001.5 Sectio	n 5: Hydromist Venturi Stage & Booster Pump Skid
501.001.6 Sectio	n 6: Venturi Mist Elimination Stage
501.001.7 Sectio	n 7: Start up, Operation, and Servicing
501.001.8 Sectio	n 8: Recommended Spare Parts
	n 9: Appendix A – Envirocare Costumer Drawings
	on 10: Appendix B – Primary Equipment Catalogs
	Duplex Basket Strainer
501.001.10.2	Venturi Water Feed Booster Pump & Operational Curve
501.001.10.3	Check Valve
501.001.10.4	Back Pressure Relief Valve (Safety Valve)
501.001.10.5	3-Piece Isolation Valve (Booster Pump Skid)
501.001.10.6	Orifice Flowmeter
501.001.10.7	Drawings



501.001 Operation & Maintenance Manual

Operation & Maintenance Manual for the

HydroMist VenturiPak TM

Off-Gas Wet Scrubbing System

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Revision Date: January 22, 2001

OPERATION AND MAINTENANCE MANUAL

OUTLINE

HydroMist VenturiPak [™] Wet Scrubber Introduction
Sub-Cooler Impingement Tray Stage
Condenser Mist Eliminator Stage
Venturi Impingement Tray Stage4
HydroMist Venturi Stage & Booster Pump Skid5
Venturi Mist Eliminator Stage 6
Start up, Operation & Servicing7
Recommended Spare Parts8
Appendix A – EnviroCare Customer Drawings9
Appendix B Primary Equipment Catalogs

	HydroMist VenturiPak [™] Wet Scrubber Introduction	NAKASE KERKATUL
2	Sub-Cooler Impingement Tray Stage	
3	Condenser Mist Eliminator Stage	
4	Venturi Impingement Tray Stage	
5	HydroMist Venturi Stage & Booster Pump Skid	
6	Venturi Mist Eliminator Stage	
7	Start up, Operation & Servicing	
8	Recommended Spare Parts	
9	Appendix A – EnviroCare Customer Drawings	用源的图光级图
10	Appendix B – Primary Equipment Catalogs	



501.001.1 Section 1: Hydromist Venturipak Wet Scrubber Introduction

OPERATION AND MAINTENANCE MANUAL

SECTION 1

HYDROMIST VENTURIPAK™ WET SCRUBBER INTRODUCTION

HYDROMIST VENTURIPAK™ SCRUBBER SYSTEM

The VenturiPak[™] scrubber system (U.S. Patent 5,279,646 and patents pending) consists of a multiple impingement scrubber / sub-cooler stages, a venturi stage, and a high efficiency mist eliminator stage. The venturi stage consists of multiple venturi elements combined with counter airflow water sprays centered at each venturi throat inlet. Each venturi element is removable to provide flexibility in scrubbing performance and application. The HydroMist VenturiPak[™] scrubber system is an improved venturi scrubber system which provides high efficiency, adjustable scrubbing of sub-micron and condensable particulate by:

- 1. Sub-cooling and condensing condensable gases <u>prior</u> to the venturi scrubbing stage.
- 2. Providing pre-atomization of the venturi stage water via proprietary high-pressure water spray nozzles.

The HydroMist VenturiPak™ Scrubber System consists of:

- 1. Two- (2) Under Tray Spray Lances with two- (2) EnviroCare SpiralMist nozzles per lance.
- 2. Two- (2) Dual-Orifice™ sub-cooler impingement trays.
- 3. One- (1) Vane Type Condenser Mist Eliminator at recycle gas discharge.
- 4. Two- (2) Condenser Mist Eliminator Spray Lances each with two- (2) EnviroCare-RainDrop nozzles.
- 5. One- (1) Dual-Orifice™ venturi impingement tray.
- 6. Split Gas Flow: Under design conditions 24,422 ACFM of off-gas @ 132°F & 10.5% by volume moisture recycles back to the dryer after flowing through the condenser mist eliminator. 7,047 ACFM @ 105°F flows through the venturi impingement tray then onto the venturi stage.
- 7. The HydroMist venturi stage contains five- (5) HydroMist Venturi assemblies each with a 3/8" MPT water feed port. Each venturi assembly includes one- (1) EnviroCare SpiralMist venturi nozzle.
- One- (1) Venturi Water Feed Lance with internal and external connection nipples and accessories to connect to venturi assembly water feed port.
- 9. One- (1) Mesh Type Venturi Stage Mist Eliminator at the discharge of the venturi stage shell.

- One- (1) venturi Stage Mist Eliminator Spray Lance with two- (2) EnviroCare SpiralMist nozzles.
- 11. One- (1) Booster Pump Skid with high-pressure water pump & accessories sized to supply sufficient water pressure and flow to the venturi assemblies.

The HydroMist VenturiPak[™] scrubber for this application is configured as shown on EnviroCare's process & instrumentation drawing C100-6079 and general arrangement drawing C500-6079, reduced copies of both can be found in Appendix A. Appendix A also includes drawings for all of the major components of the HydroMist VenturiPak[™] off-gas scrubbing system.

The system includes a sub-cooler impingement tray stage, a condenser mist eliminator stage, a venturi impingement tray stage, a HydroMist venturi stage & booster pump skid and venturi mist eliminator stage. Water flows and gas conditions for all stages are shown on drawing C100-6079. (Appendix A)

Details for each stage can be found in the remaining sections of this manual.



501.001.2 Section 2: Sub-Cooler Impingement Tray Stage

OPERATION AND MAINTENANCE MANUAL

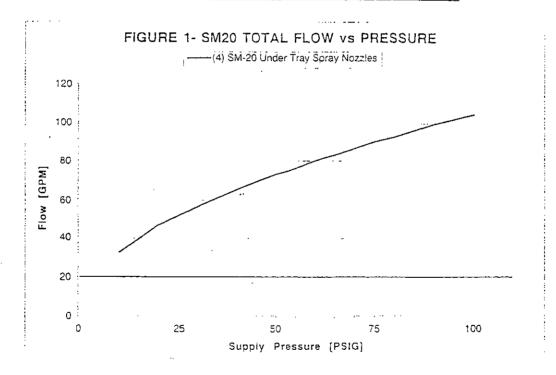
SECTION 2

SUB-COOLER IMPINGEMENT TRAY STAGE

SUB-COOLER IMPINGEMENT TRAY STAGE

The sub-cooler stage is comprised of two- (2) under tray spray lances with two- (2) SpiralMist spray nozzles on each lance and two levels of impingement trays each with one- (1) Dual-Orifice™ impingement tray. The under tray spray nozzles spray upward and are sized to supplement the cooling of the incoming gases (saturating the gases), to capture larger particles and to wash the bottom of the lower impingement plate (preventing build-up). Some of the spray water is carried into the lower tray section where it adds to the tray water flow. The under tray spray nozzles are connected to "low pressure" plant water and should operate at no less than 40 psig. See drawing C112-6079 in Appendix A for lance design details. A water flow curve for the under tray spray nozzles is shown below (Figure 1). PERIODIC INSPECTION OF THE TRAY SPRAY NOZZLES IS

RECOMMENDED TO CHECK FOR CLOGGING AND/OR WEAR.



The impingement tray stages form droplets as the gases pass through the flooded Dual-Orifice™ impingement trays. The interaction between the droplets and the gas results in the collection of the smaller particulate (down to 2 micron) and sub-cooling of the gas stream. Sub-cooling causes water vapor and condensable gases in the saturated gas stream to condense into a collectable particulate. The condenser tray water flow should be set at no less than 468 gpm ensuring that the gases exiting the condenser and being recycled back to the dryer do not exceed 130 ° F but should not drop below 125°F. PERIODIC INSPECTION OF THE PLATES IS RECOMMENDED TO CHECK FOR CLOGGING OR THE ACCUMULATION OF MATERIAL.



501.001.3 Section 3: Condenser Mist Eliminator Stage

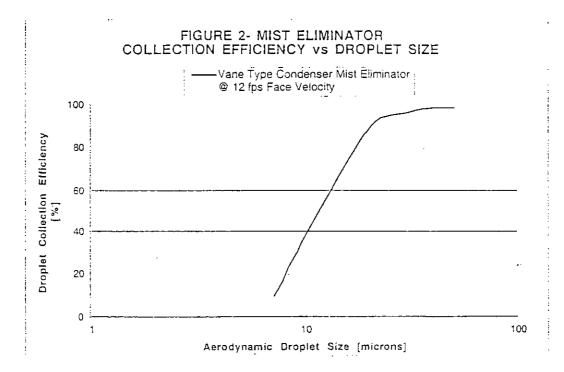
OPERATION AND MAINTENANCE MANUAL

SECTION 3

CONDENSER MIST ELIMINATOR STAGE

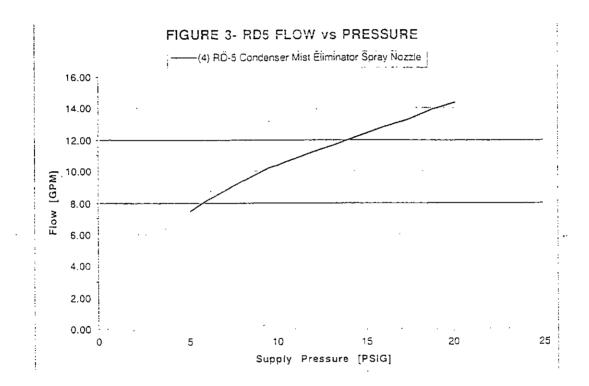
CONDENSER MIST ELIMINATOR STAGE

The Condenser Mist Eliminator is located at the recycle gas discharge of the condenser shell. The system design calls for approximately 75% of the gas flow that exits the sub-cooler impingement tray stage to recycle back to the dryer via the condenser mist eliminator stage. This vane type, 316-SS, sectional mist eliminator is designed for maximum collection of entrained water droplets from the sub-cooler impingement tray stage. This unit provides droplet separation and collection over a wide range of gas flow velocities, typically 75-100% of design. A typical droplet collection efficiency curve (Figure 2) for this style moisture removal device is shown below.



The mist eliminator is divided into four- (4) sections for ease of installation and maintenance.

Two Condenser Mist Eliminator spray lances are included downstream of the vane type mist eliminator. Each lance includes two- (2) RainDrop spray nozzles centered over the mist eliminator to provide continuous washing with clean water. Continuous washing prevents particle build up by ensuring proper drainage of captured particulate laden droplets from the mist eliminator vanes under various operating conditions. See drawing C114-6079 Appendix A for lance design details. The nozzle is connected to "low pressure" potable water through a pressure reduction valve, which should be set to supply approximately 7psig of water pressure to the lance. A water flow curve for the lance can be found below. (Figure 3)



PERIODIC INSPECTION OF THE SPRAY NOZZLE AND VANE MIST ELIMINATOR FOR CLOGGING AND WEAR IS RECOMMENDED.



501.001.4 Section 4: Venturi Impingement Tray Stage

OPERATION AND MAINTENANCE MANUAL

SECTION 4

VENTURI IMPINGEMENT TRAY STAGE

VENTURI IMPINGEMENT TRAY STAGE

The system design calls for the remaining 25% of the gas flow that exits the subcooler impingement tray stage to flow through the venturi impingement stage and then onto additional particulate removal stages before exiting the system via the venturi stage ID fan and outlet stack. The venturi impingement tray stage is comprised one- (1) Dual-Orifice™ impingement tray. The impingement tray stage forms droplets as the gases pass through the flooded Dual-Orifice™ impingement tray. The interaction between the droplets and the gas results in the additional collection of the smaller particulate (down to 2 micron) and additional sub-cooling of the gas stream. The additional sub-cooling causes more water vapor and condensable gases in the saturated gas stream to condense. The venturi tray water flow should be set at no less than 135 gpm ensuring that the gases entering the HydroMist venturi stage do not exceed 105 °F. PERIODIC INSPECTION OF THE PLATE IS RECOMMENDED TO CHECK FOR CLOGGING OR THE ACCUMULATION OF MATERIAL.



501.001.5 Section 5: Hydromist Venturi Stage & Booster Pump Skid

OPERATION AND MAINTENANCE MANUAL

SECTION 5

HYDROMIST VENTURI STAGE & BOOSTER PUMP SKID

HYDROMIST VENTURI STAGE

The HydroMist Venturi Stage captures the residual fine, sub-micron particulate including condensable constituents that penetrate the impingement stages. The venturi stage consists of a solid venturi diaphragm with mounting locations for five- (5) HydroMist venturi assemblies. The venturi stage also includes one- (1) Venturi Water Feed Lance, which includes all the accessories necessary to connect the high-pressure water supply from the Booster Pump Skid to the venturi assemblies.

An illustration of the venturi assembly can be found on the following page. (Figure 4) The HydroMist venturi assembly consists of the mounting plate, low energy loss inlet, throat, outlet cone assembly, feed water connection & outlet deflector plate.

The mounting plate is oversized to allow for fabrication of the venturi assembly in one piece. This allows the assembly to be installed and removed through the access door above the venturi mounting plate diaphragm. The venturi flange bolts to the top of the venturi stage diaphragm. Neoprene gaskets are provided between the venturi flange and the mounting plate to prevent gas leakage or bypass.

The venturi water feed lance is fabricated in two pieces. The exterior connection and accessories allow for connection to supply piping that runs from the Booster Pump Skid. The interior connections and accessories allow for mating of the feed lance to the venturi assembly via a high-pressure hose. The water feed tubing in the venturi assembly runs the length of the venturi and feeds the venturi spray nozzle. Each venturi includes one-(1) SpiralMist spray nozzle that injects atomized water counter current to the process gas flow. This design provides an elevated relative velocity differential between the water and particulate laden gas stream, and thus the HydroMist venturi stage produces extremely high particulate collection efficiencies. The spray lance to venturi assembly connection details are shown in detail on drawing C110-6079. (Appendix A) The recommended operating pressures for the venturi water feed lance is 200psig. The water connection for the spray lance (as well as all other lances) is accomplished via a flexible metal hose with a hand isolation valve. All lances include a pressure gauge to provide operating pressure indication. PERIODIC INSPECTION OF THE VENTURI SPRAY NOZZLES IS RECOMMENDED TO CHECK NOZZLE CLOGGING AND/OR WEAR. Frequency depends on the quality of water supplied to the Booster Pump Skid, but should be performed at least bi-annually.

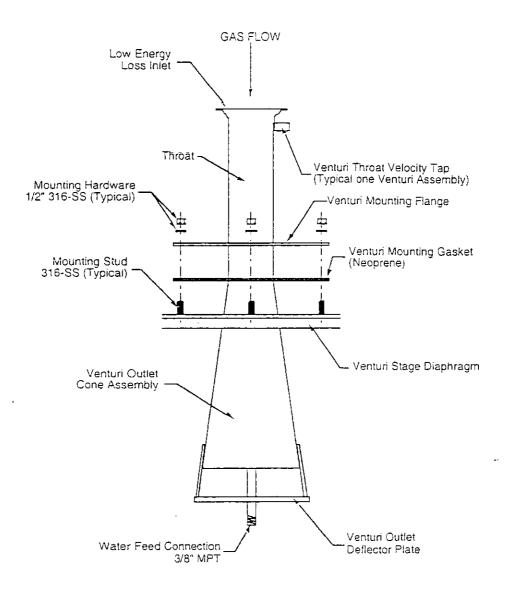
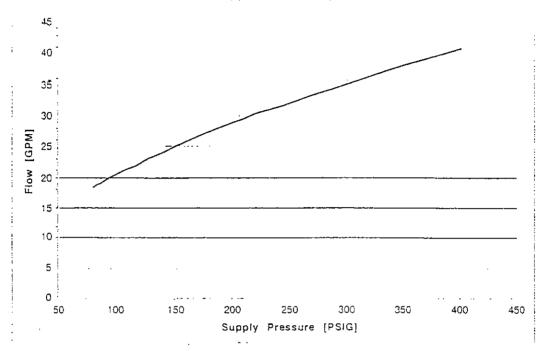


FIGURE 4- HYDROMIST VENTURI ASSEMBLY

Figure 5 shows the water flow curve for the SpiralMist venturi spray nozzles.

FIGURE 5- SM8 FLOW vs PRESSURE

--- (5) ŚM-8 Venturi Spray Nozzies



Several inches below the outlet cone assembly a mist deflector arranged to deflect the scrubbed process gases and spray mist. These deflectors are designed to cause the mist from the venturi outlet cones to agglomerate into droplets which fall into the venturi shell bottom and pass to drainage. The deflector plates deflect the fog and captured particulate passing through the venturi cones. Any residual liquid mist is captured in the mist eliminator stage. It is covered in the Venturi Mist Eliminator Stage section.

BOOSTER PUMP SKID

The Booster Pump Skid (shown on drawing C200-6079) contains the high-pressure pump necessary to boost the venturi water supply to the necessary pressure. "Low-Pressure" plant water (40psig) is enters the skid through a dual basket water strainer. The basket strainer's perforated screen basket is sized to remove debris in the feed water that would otherwise clog the venturi spray nozzles. PERIODIC CLEANING OF THE OPERATING BASKET SHOULD BE COMPLETED. Frequency depends on the quality of water supplied to the Booster Pump Skid, but should be performed at least bi-weekly. The water continues through the water piping, or water train, and into a water booster pump. Here the water pressure is increased to 200 psig depending on the inlet water pressure. The now high-pressure water flows through a check valve then an orifice style flow meter. The flow meter includes a local display and a 4-20mA analog signal for customer remote display as desired.

The booster pump skid also includes pressure indicators at the inlet and outlet of the pump. These should be checked periodically to ensure the pump is providing adequate boost to the pressure. To ensure efficient particulate collection at the venturi stage, the pressure at the discharge of the pump should never drop below 210 psig, and the pressure at the venturi water feed lance should never drop below 200 psig. The skid includes one safety feature to ensure the pump does not operate below its minimum required water flow. A pressure regulating valve is installed downstream of the pump. It is field set to provide pressure relief and water flow if the pump should experience a deadhead operating condition.

Gas flow through the venturi stage is measured continuously by measuring differential pressure between venturi inlet and throat. 1/4" FPT tapped ports are included on one venturi assembly and on the side of the tank for this device. Typically pressure drop across the venturi diaphragm is also measured, and 1/4" FPT ports are included on the shell for this connection as well. Any pressure taps that are not being used should be plugged during operation.

Note: The Booster Pump Skid requires no adjustments during normal operation. However, pressure & flow values for all components on the booster pump skid and the rest of the HydroMist VenturiPak[™] off-gas scrubbing system should be logged every hour as an operational log. The recommended operating parameters for the entire scrubber system can be found on drawing C100-6079. (Appendix A) See figure 6 below for a diagram of the Booster Pump Skid.

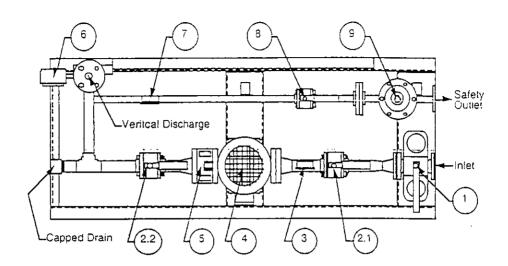


FIGURE 6 - BOOSTER PUMP SKID

Item No.	Description
1	1 1/2" Duplex Basket Strainer
2.1 & 2.2	1 1/4" Ball Valve
3	Pressure Gauge (0-160 psig)
4	Booster Pump (5hp / 480 Volt / 3 Phase / 60 Hz)
5	1 1/4" Check Valve
6 .	Orifice Flow Meter (0-40gpm local display & 4-20mA output)
7	Pressure Gauge (0-300 psig)
8	3/4" Ball Valve
9	3/4" Back-Pressure Regulating Valve (Safety Valve)



501.001.6 Section 6: Venturi Mist Elimination Stage

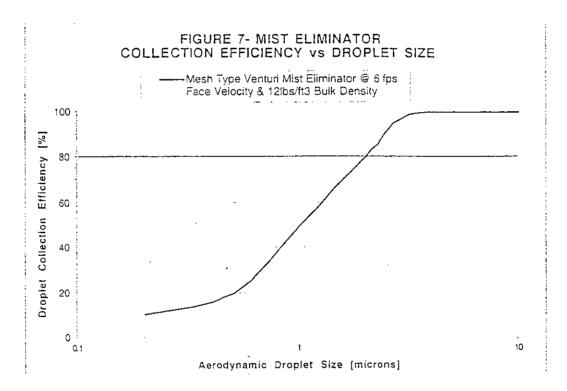
OPERATION AND MAINTENANCE MANUAL

SECTION 6

VENTURI MIST ELIMINATOR STAGE

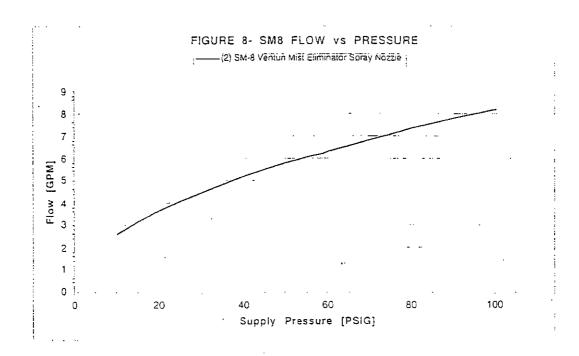
VENTURI MIST ELIMINATOR STAGE

The Venturi Mist Eilminator is located at the discharge of the venturi shell. This mesh type, 316-SS, single piece mesh pad is of an ultra efficient design for maximum collection of fine entrained droplets from the venturi stage. The mesh type mist eliminator provides excellent fine droplet separation and collection over a wide range of gas flow velocities, typically 40-100% of design. The graduated density mesh allows for superior separation of droplets laden with particulate and drainage preventing plugging of the pad without sacrificing separator efficiency. A typical droplet collection efficiency curve (Figure 7) for this style pad is shown below.



The Venturi Mist Eliminator is installed in a horizontal duct housing extending from the venturi shell. The housing includes a flange access port centered directly above the mesh housing for ease of maintenance and installation.

One Venturi Mist Eliminator spray lance is included just upstream of the mesh type mist eliminator. The lance includes two- (2) SpiralMist spray nozzles in front of the mist eliminator to provide continuous washing with clean water. Continuous washing prevents particle build up by ensuring proper drainage of captured particulate laden droplets from the mist eliminator mesh under various operating conditions. See drawing C111-6079 (Appendix A) for lance design details. The lance is connected to a "low pressure" potable water supply and should operate at no less than 40 psig. A water flow curve for the lance can be found below. (Figure 8)



PERIODIC INSPECTION OF THE SPRAY NOZZLE AND MESH MIST ELIMINATOR FOR CLOGGING AND WEAR IS RECOMMENDED.



501.001.7 Section 7: Start up, Operation, and Servicing

OPERATION AND MAINTENANCE MANUAL

SECTION 7

START-UP, OPERATION, AND SERVICING

START-UP, OPERATION AND SERVICING

Scrubber Start-Up and Operation

The following sequence must be followed at start-up:

- 1. Verify all valves open as necessary to allow water flow to system.
- 2. Turn on water flow to the sub-cooler impingement trays.
- 3. Turn on water flow to the venturi impingement tray.
- 4. Turn on water flow to the under tray spray lances.
- 5. Turn on water flow to the condenser mist eliminator spray lance.
- 6. Turn on water flow to the HydroMist venturi assemblies. Energize the booster pump to elevate venturi feed water pressure.
- 7. Allow water to flow for 5 minutes to ensure all water boxes and water seals are filled before activating ID fans.
- 8. Begin process gas flow through scrubber.
- 9. Energize venturi stage ID fan. (Fan and controls by others.)
- 10. Turn on water flow to the venturi mist eliminator spray lance.
- 11. Using drawing C100-6079 from appendix A as a guide, verify that all pressures and water flows are at a minimum as detailed on drawing.
- 12. Walkthrough system and verify all access doors are sealed completely.
- 13. System should operate with very minimal changes. Condenser water flow may be varied to keep the recycled air temperature above 125°F but below 130°F.

Scrubber Shutdown

The following sequence must be followed at shutdown:

- Shut off process gas flow through scrubber.
- Allow water to run for 10 minutes after ID fans have finished spinning.
- 3. Turn off venturi feed water booster pump.
- 4. Turn off supply water to each location.

Inspection

Inspection of the equipment should be made as outlined below to keep operating efficiency at optimum conditions.

- •1. Pressure gauges should be observed daily for proper operating pressure, compared for accuracy of readings and replaced if necessary.
- 2. All spray nozzles should be periodically checked for clogging or wear.
- 3. Line strainers should be blown down daily and cleaned as required.
- 4. Tray and mist eliminator seals should be checked for clogging or the accumulation of material any time gas flow is shut down.

Trouble Shooting

Most operational problems associated with the HydroMist venturi scrubber stem from improper distribution of water. Many of the problems lead to or show up in the form of impingement tray plugging. Plugging is always the result of another condition or failure and does not begin without some other cause. The following chart outlines the types of problems that can be encountered and how to correct these problems.

Table I. Plugging -- First Impingement Tray

1 db10 1: 1,459.15	
Lack of Spray Water	Check water pressure.
	Check for clogged under tray spray nozzles.
	Check strainer.
Low Plate Water Level	Increase water flow rate.
Improper Water Distribution	Level the impingement trays.
	Adjust internal weirs for even overflow across width of plate.
Material Adhering to Underside of Tray	Increase under tray spray water flow.

Table II. Plugging -- All Impingement Trays

Re-circulation of Solids in Water System	Limit the percent of solids in the tray water to 5% by weight. Check for clogged spray nozzles.
Low Plate Water Level	See Table I.
Improper Water Distribution	See Table I.

Table III. Low Efficiency -- Excessive Particulate Emission from Scrubber

Table III. Low Little IIIcy Excessive Familiarie Emission from Schubber		
See Table I.		
Check fan performance and adjust to		
design volume.		
Check fan performance and adjust to design volume.		
Check booster pump operation.		
Verify sufficient inlet pressure to booster pump skid.		
Check duplex basket strainer on skid.		
Check supply piping and strainers for plugging.		

Table IV. Low Gas Flow Volume

Check items under Tables I. and II.	See Tables I. and II.
Check pressure drop reading across	Install differential pressure gauges for
impingement stages.	operator observance.
Check fan performance against design data	Adjust as required.
Check duct design system	Remove unnecessary system resistance or adjust fan performance as required.

Table V. Water Carryover

Table V. Water Carryover	
Check tray drains for clogging. Clogging prevents normal drain of water, allowing carry-over and re-entrainment in air stream.	Clean out drains for normal flow.
Excessive Air Volume	Check against design data.
Condenser Mist Eliminator Supply Pressure to high	Check pressure regulator setting
Change condenser mist eliminator spray nozzle location from downstream of vane (above) to upstream (below)	Contact EnviroCare for instructions.

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Table VI. Surging -- Pulsating airflow, loss of suction

Water flow too high across trays more than drain can accommodate.	Adjust water flow down.
Frozen or plugged venturi stage drain seals.	Provide weep holes or drain to prevent freezing. Clean drains.
By passing tray seals.	Clean out seals of accumulated material.

Table VII. High Pressure Drop Across Impingement Trays (>5" △P)

Water Flow too high across plates	Adjust water flow. Adjust water box weirs.
Plugging	See Tables I. and II.
Excessive Air Volume	Measure and adjust.

Table VIII. High Pressure Drop Across Mist Eliminator Pad (>4" ΔP)

Check for material build-up	l Clean as required.
Il Check for material build-up	i Ciedii as regulied.
I Check to material build-up	1 010011 00 104011 001

Table IX. High Pressure Drop Across Inlet or Outlets

Check sizes of ducts	Modify as required.
Check for restrictions	Modify as required
Be sure readings are accurate and taken	Install pressure differential gauges for
properly	operator observance.

Table X. Scrubber Drain Connections

Bypassing drain seals or loss of seal	Drains should be sealed or trapped against differential pressure between scrubber and atmosphere as well as between scrubber stages.
Water build-up in bottom cones	Check for clogging, restricting drain connection, or loss of seal.



ENVIRONMENT AND PROCESS TECHNOLOGIES

501.001.8 Section 8: Recommended Spare Parts

EnviroCare *HydroMist VenturiPak*TM Wet Scrubber Operation & Maintenance Manual

OPERATION AND MAINTENANCE MANUAL

SECTION 8

RECOMMENDED SPARE PARTS

EnviroCare *HydroMist VenturiPak*TM Wet Scrubber Operation & Maintenance Manual

RECOMMENDED SPARE PARTS NOTE: QUANTITIES LISTED ARE FOR EACH UNIT (1 OF 4)

HydroMist Venturi & Water Feed Lance

Part No.	Size	Qty.	Part Description
B110-6079-3	1 1/2"	1	QUICK CONNECT COUPLING (SOCKET X FPT)
B110-6079-4	1 1/2"	1	QUICK CONNECT COUPLING (PLUG X MPT)
B110-6079-18	1 1/2"X48"	1	HIGH-PRESSURE EXTERIOR FEED HOSE
B110-6079-19	1 1/2"	1	BALL VALVE
B110-6079-21	1 1/2""	1	Y-STRAINER PERFORATED SCREEN INSERT
B110-6079-24	1/4"	1	PRESSURE GAUGE, 0-400 PSIG, 2 1/2" DIAL
B110-6079-29	1/2"X48"	2	HIGH-PRESSURE INTERIOR FEED HOSE
B541-6079-00	4"OD	1	HYDROMIST™ VENTURI ASSEMBLY
B541-6079-2A	1/4"	5	SPIRALMIST-8 VENTURI SPRAY NOZZLE
B541-6079-11		1	VENTURI MOUNTING GASKET (NEOPRENE)

Venturi Mist Eliminator Spray Lance

Part No.	Size	Qty.	Part Description
B111-6079-2	1/4"	2	SPIRALMIST-8 VENTURI M.E. SPRAY NOZZLE
B111-6079-4	3/4"	1	QUICK CONNECT COUPLING (MPT X F-CAM)
B111-6079-5		1	LANCE MOUNTING GASKET (NEOPRENE)
B111-6079-12	1/4"	ົ້ 1	PRESSURE GAUGE, 0-100 PSIG, 2 1/2" DIAL
B111-6079-14	3/4"X48"	1	FLEX HOSE
B111-6079-15	3/4"	1	QUICK CONNECT COUPLING (FPT X M-CAM)
B111-6079-16	3/4"	1	BALL VALVE

Under Tray Spray Lance

Part No.	Size	Qty.	Part Description
B112-6079-2	3/8"	4	SPIRALMIST-20 UNDER TRAY SPRAY NOZZLE
B112-6079-4	1"	1	QUICK CONNECT COUPLING (MPT X F-CAM)
B112-6079-5		2	LANCE MOUNTING GASKET (NEOPRENE)
B112-6079-12	1/4"	2	PRESSURE GAUGE, 0-100PSIG, 2-1/2" DIAL
B112-6079-14	1"X48"	2	FLEX HOSE
B112-6079-15	1"	1	QUICK CONNECT COUPLING (FPT X M-CAM)
B112-6079-16	1"	2	BALL VALVE

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Condenser	Mist	Eliminator	Spray	<u>Lance</u>

Part No.	Size	Qty.	Part Description
B114-6079-2	1/2"	1	RAINDROP-5 CONDENSER M.E. SPRAY NOZZLE
B114-6079-4	3/4"	1	QUICK CONNECT COUPLING (MPT X F-CAM)
B114-6079-5		1	LANCE MOUNTING GASKET (NEOPRENE)
B114-6079-12	1/4"	1	PRESSURE GAUGE, 0-60PSIG, 2-1/2" DIAL
B114-6079-14	3/4"X48"	1	FLEX HOSE
B114-6079-15	3/4"	1	QUICK CONNECT COUPLING (FPT X M-CAM)
B114-6079-16	3/4"	1	BALL VALVE
B114-6079-17	3/4"	1	HIGH-PRESSURE REGULATING VALVE, 2-10 PSIG

Booster Pump Skid

Part No.	Size	Qty.	Part Description
B200-6079-1	1 1/2"	2	STRAINER BASKETS, STAINLESS STEEL
B200-6079-2		1	VERTICAL PUMP REPAIR KIT
B200-6079-3	1 1/4"	1	SPRING LOADED CHECK VALVE
B200-6079-4	3/4"	1	BACK PRESSURE RELIEF VALVE REPAIR KIT
B200-6079-5	3/4"	1	FULL PORT BALL VALVE REPAIR KIT
B200-6079-6	1 1/4"	2	FULL PORT BALL VALVE REPAIR KIT
B200-6079-7	1"	1	ORIFICE FLOW METER
B200-6079-8	1/4"	2	PRESSURE GAUGE, 0-160 PSIG, 2 1/2" DIAL
B200-6079-9	1/4"	2	PRESSURE GAUGE, 0-300 PSIG, 2 1/2" DIAL

Miscellaneous Items

Part No.	Size	Qty.	Part Description
B590-6079-00	37"x81"	2	ECS SUB-COOLER IMPINGEMENT TRAY
B590-6079-0	30"x50"	1	ECS VENTURI IMPINGEMENT TRAY
B530-6079-1	72" x 72"	1	CONDENSER MIST ELIMINATOR
B543-6079-1	60"x48"	1	VENTURI STAGE MIST ELIMINATOR



ENVIRONMENT AND PROCESS TECHNOLOGIES

501.001.9 Section 9: Appendix A - Envirocare Customer Drawings

EnviroCare HydroMist VenturiPakTM Wet Scrubber Operation & Maintenance Manual

OPERATION AND MAINTENANCE MANUAL

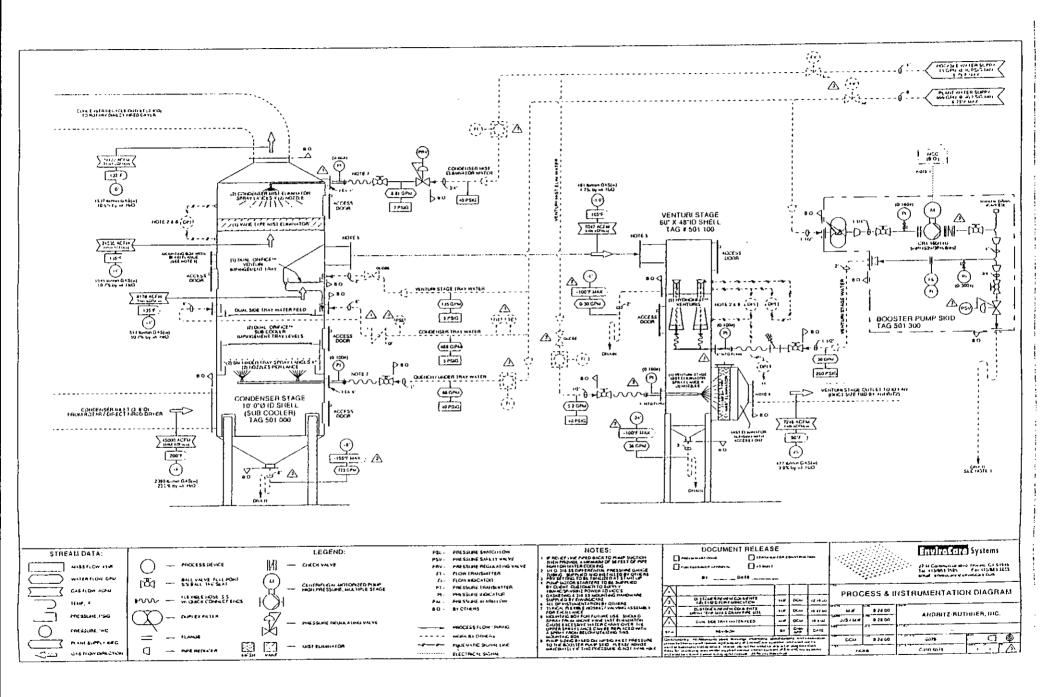
SECTION 9

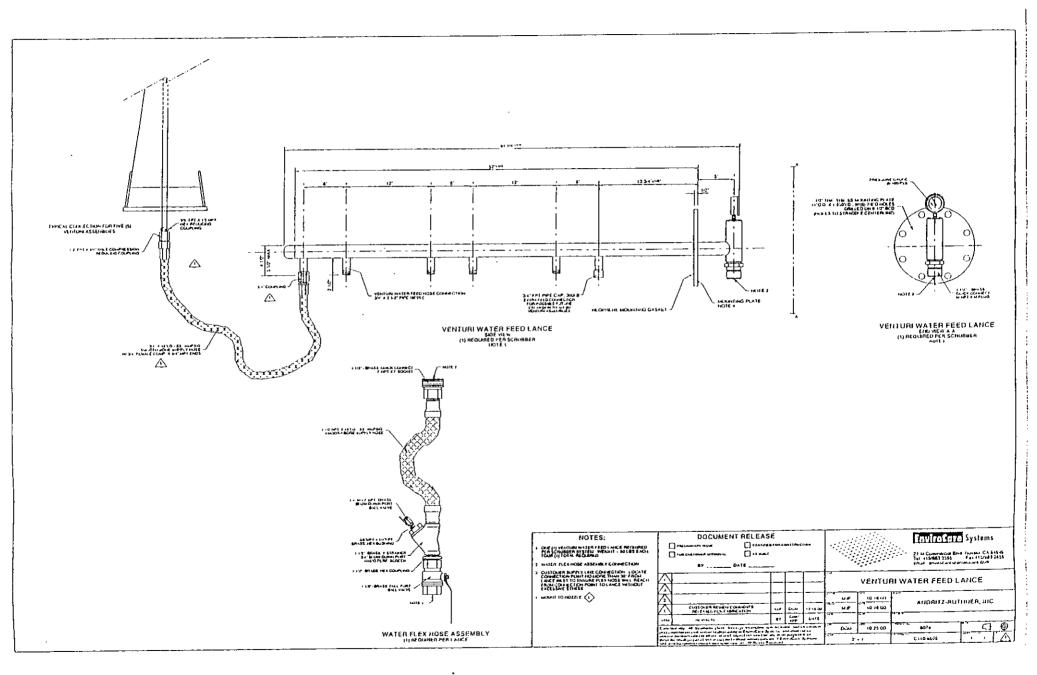
APPENDIX A

ENVIROCARE CUSTOMER DRAWINGS

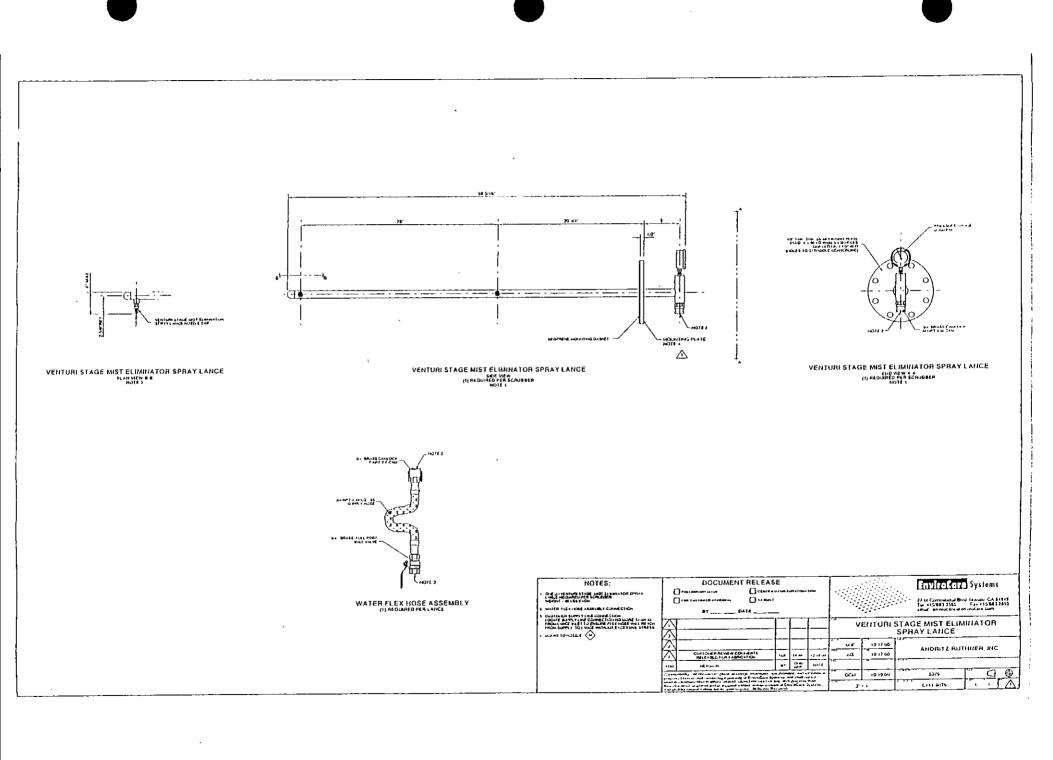
EnviroCare *HydroMist VenturiPak™* Wet Scrubber Operation & Maintenance Manual

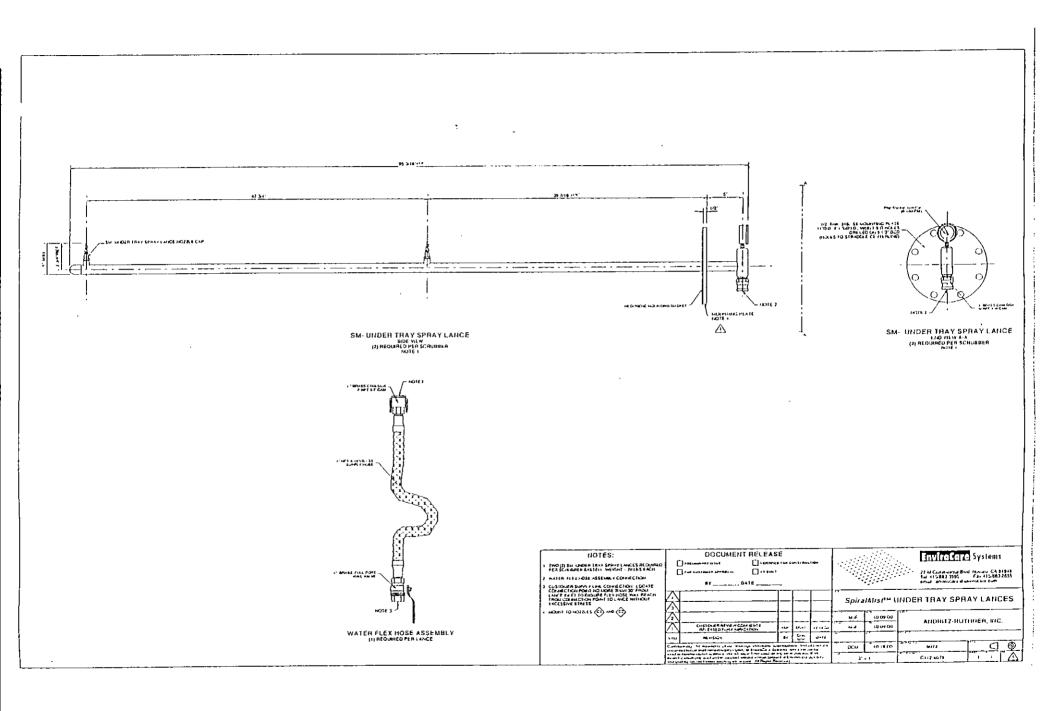
ENVIROCARE CUSTOMER DRAWINGS (11" x 17" reduced copies)	
Process & Instrumentation Drawing	C100-6079
Venturi Water Feed Lance	C110-6079
Venturi Stage Mist Eliminator Spray Lance	C111-6079
SpiralMist under Tray Spray Lances	C112-6079
Condenser Mist Eliminator Spray Lance	C114-6079
Booster Pump Skid – General Arrangement	C200-6079
HydroMist VenturiPak™ General Arrangement	C500-6079
HydroMist VenturiPak™ General Arrangement (Mirror)	C501-6079
Flange and Anchoring Details	C505-6079

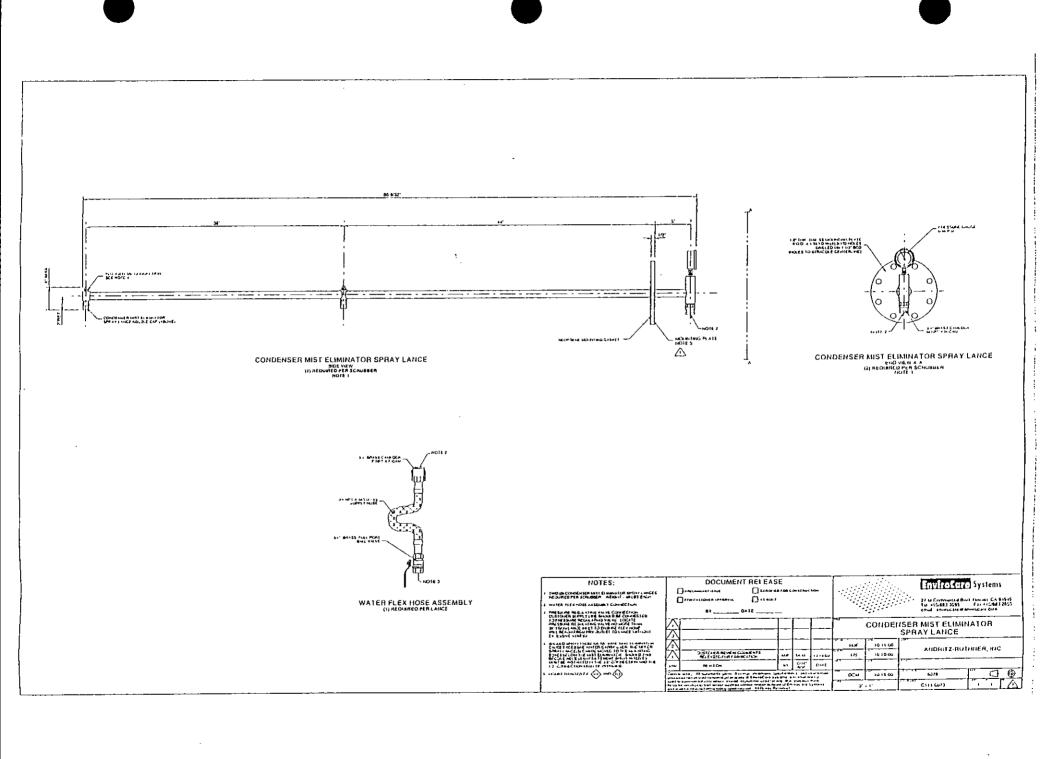


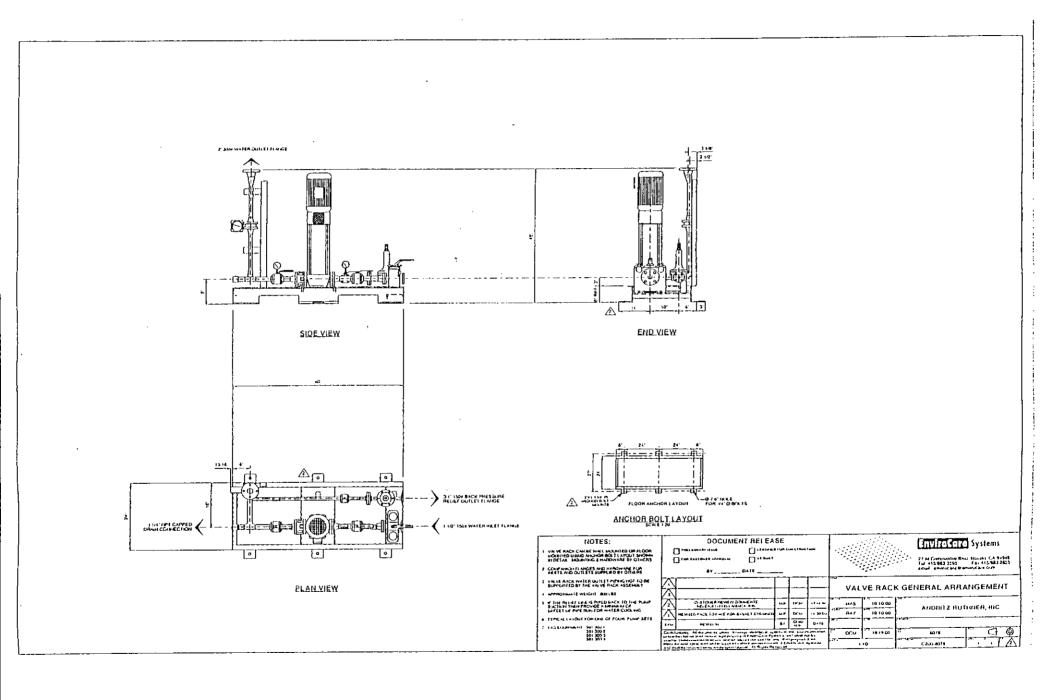


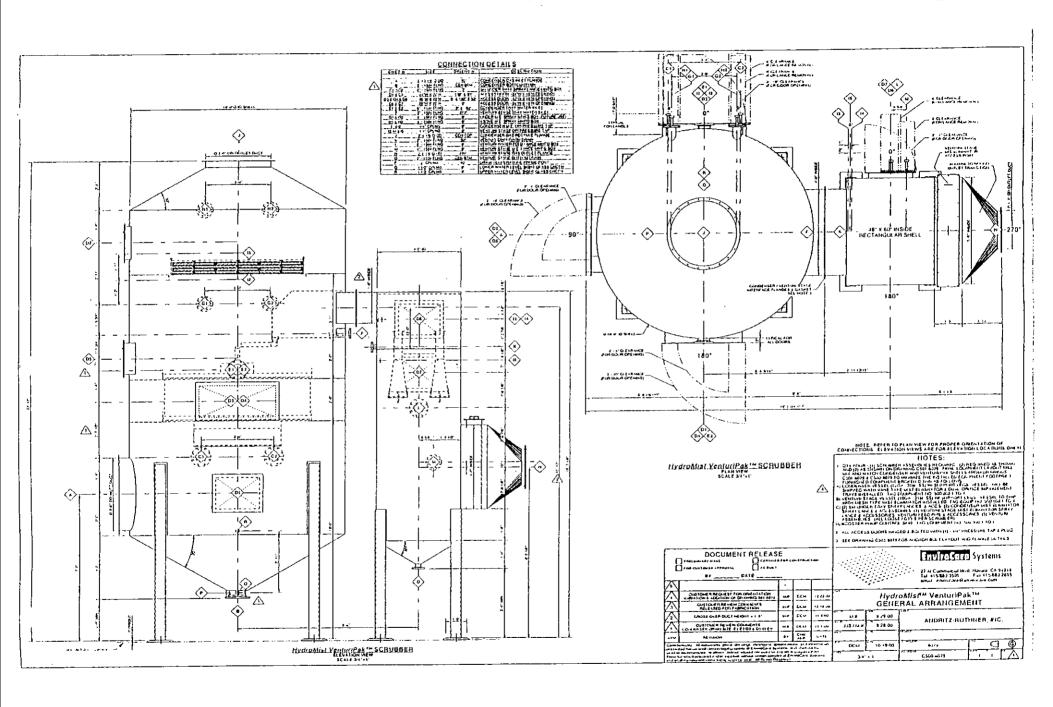
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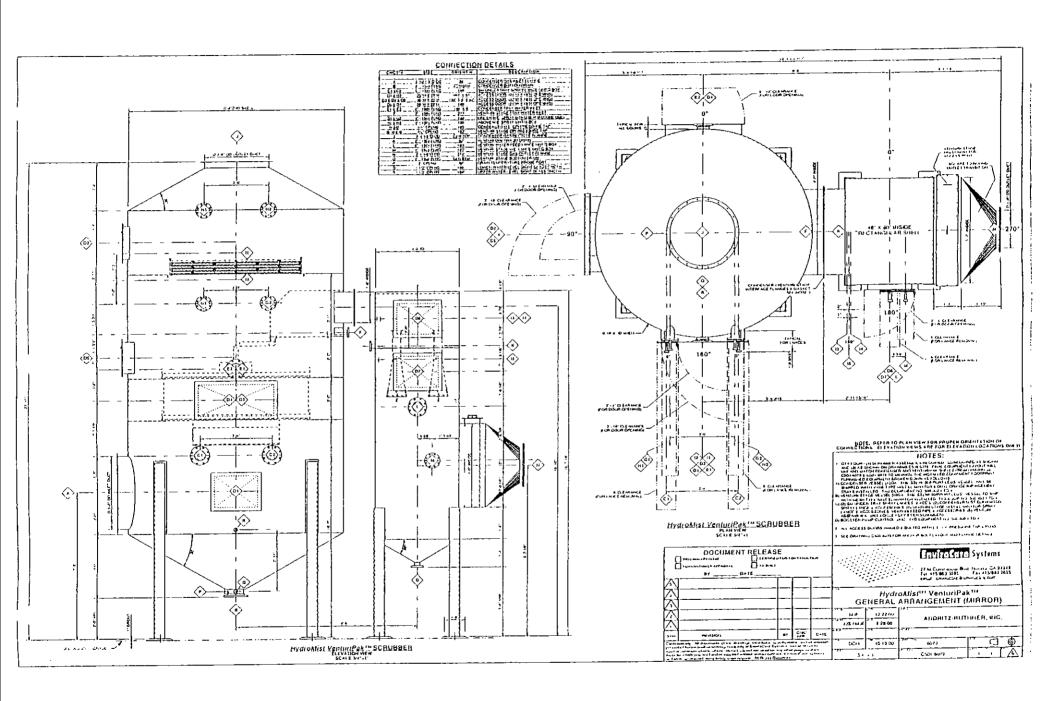


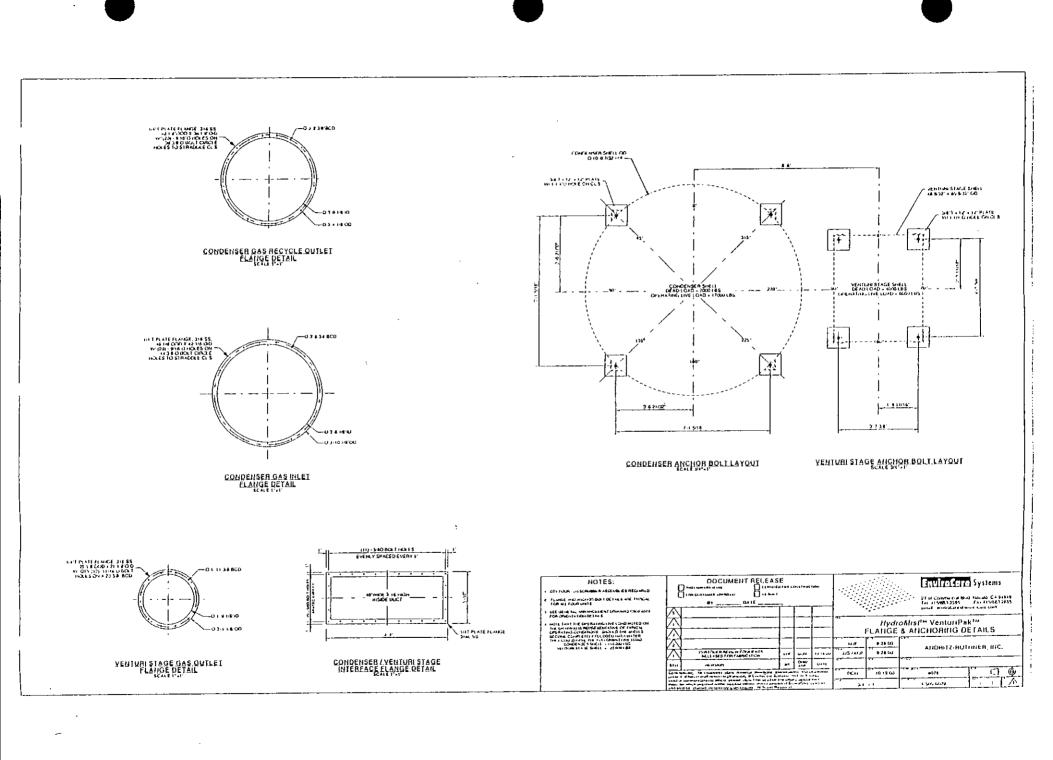












Operation and Maintenance Manual for Regenerative Thermal Oxidation System



ABATEMENT SYSTEMS, INC.

Proposal For A

Regenerative Thermal Oxidation System

Andritz-Ruthner, Inc.

Prepared By:

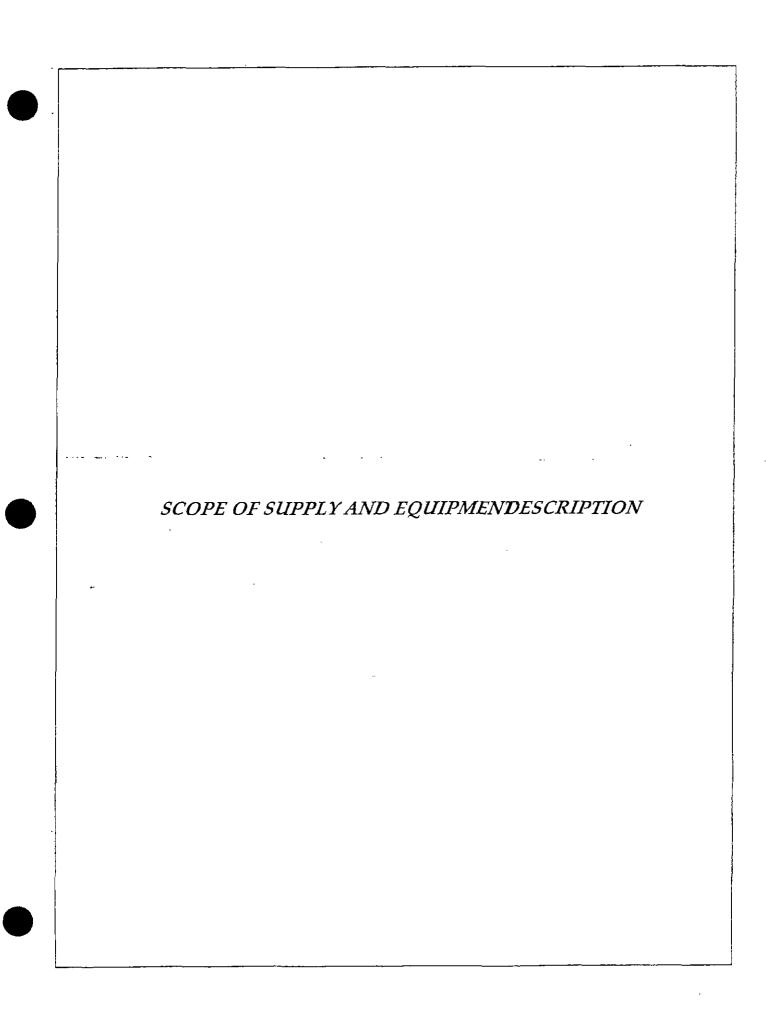
CECO Abatement Systems, Inc.

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A CECO ENVIRONMENTAL COMPANY

TABLE OF CONTENTS

SCOPE OF SUPPLY AND EQUIMENT DESCRIPTION	.3
WORK BY PURCHASER	.10
CLARIFICATIONS AND EXCEPTIONS	.12
PRICING/COMMERCIAL	14
TERMS AND CONDITIONS	.19
MAINTENANCE SCHEDULES & RECOMMENDED SPARE PARTS	.22
TECHNICAL DATA	.25



OXIDATION EQUIPMENT DESCRIPTION

CECO Abatement Systems proposes to furnish one (1) turnkey, Regenerative Thermal Oxidation (RTO) system

This system is designed to achieve 98% VOC destruction efficiency. This type of system has the unique ability to maintain 95% thermal efficiency while operating up to 1800 °F in the combustion chamber.

Following is a brief description of the equipment to be provided. All dimensions and design parameters are preliminary and are subject to final engineering. The proposed design is based on the CECO Abatements Systems present understanding of the process. The design basis is subject to confirmation by the buyer. As always, portions of the design are subject to change until final engineering is completed. A Process Flow Diagram (PFD) showing the flow scheme and the mass and energy balance is located in the Technical Data Section of the proposal. CECO Abatement Systems requests that you carefully review this data to insure that the basis for design is correct. Also located in the Technical Data section are the equipment specification sheets, which further detail, the scope of supply. The proposal includes skid mounting the oxidizer on a frame. By doing this, we can then mount all of the mechanical devices, piping, and electrical devices in the shop. We would then ship to the skid(s) to the jobsite for installation. In addition, we offer an installation price for the skid mounted system. In this way, we feel that Andritz's and the enduser's exposure on cost and quality are minimized.

The following is a brief summary of the proposed oxidizer system. The system that CECO Abatement Systems proposes consists of an induced draft fan and a three (3) chambered RTO. The process gases are received from the collection system tie point (assumed to be at the inlet manifold of the RTO). This gas passes through the process isolation valve before entering the inlet manifold of the RTO. Upon entering the inlet manifold, the gas passes up one heat recovery chamber (pre-heating mode), enters the combustion chamber where the VOC's are destroyed and then passes down another heat recovery chamber (heat recovery mode), and exits up the stack. The third chamber in this three (3)-chamber system is being purged of process gases in preparation to begin the pre-heating mode. Every two to three minutes the chambers are alternated from the pre-heating, purging and heat recovery modes.

Typical of combustion equipment, the oxidizer will be interlocked to provide a minimum of four (4) air changes before the burner will begin the ignition sequence during the startup of the system. To accommodate this, an isolation damper upstream of the RTO will close, separating the process from the RTO. A fresh air purge damper downstream of the isolation damper will open allowing the process gas fan to pull fresh air into the oxidizer to purge it before the burners attempt the ignition sequence. After the ignition sequence, the oxidizer will come to temperature within about four hours. Once the oxidizer reaches the temperature set point

(typically 1500 deg F), the inlet isolation damper will open and the purge damper will close. At this point, the oxidizer is fully operational.

In addition to this typical mode of operation, CECO Abatement Systems has provided a gas injection system. This system is used to artificially enhance the process gas streams heating value once the system is online. The heat content of the gas stream will be increased to approximately 2.5% of the LFL (lower flammability limt).

CECO Abatement Systems will be pleased to modify the proposed system to incorporate any special design features that the purchaser may request.

Recovery Chambers

Recovery chamber flanges will be continuously welded for airtight construction. Each recovery chamber will be internally insulated with modular, soft ceramic fiber insulation down to the support grid area. Below the support grid, the units internals will be stainless steel to prevent "wicking" of moisture from the process gas stream. It has been our experience that this phenomena is partly responsible for odor issues and corrosion at other facilities. All recovery chambers will include a recovery bed support grid fabricated from Type 304 stainless steel. The recovery chambers have been quoted as being manufactured from 1/4-inch A36 carbon steel. Because of the size of the manifolds, we have opted to place the access door below the support grid in each chamber.

Recovery Media

CECO Abatement Systems offers both traditional random saddle packing and structured "honeycomb" monolith blocks as the ceramic heat recovery media used in the regenerative heat exchanger of the RTO. Both elements are chemically and thermally stable for the typical heat-up and cool down cycles that RTO's are subjected to.

Systems that utilize monolith media have more favorable pressure drop and thermal recovery characteristics, resulting in reduced operating costs, but are more sensitive to thermal shock.

CECO Abatement Systems has had excellent success with both types of media in this application. With respect to this application, CECO Abatement Systems has chosen to use 25 x 25 cell monolithic heat exchange media because of its ability to be cleaned and its high heat exchange rate. Refer to the Equipment Specification Sheets located in the Technical Section of this proposal for information on the media included with the system.

Combustion Chamber

The combustion chamber is comprised of a single section, which is fastened to the recovery chambers. The chamber will be designed to accommodate the maximum internal pressure, which can be generated by the fan. If this cannot be accommodated economically, the system will be designed for the maximum possible operating pressure and the system will have appropriate pressure relief venting. Each combustion chamber section is insulated with soft ceramic fiber insulation designed to minimize heat loss as described in the next section. In addition, necessary burner mounting flanges and sight ports are provided to accommodate the burners provided.

Internal Insulation

The internal walls of the oxidizer are lined with soft, ceramic fiber insulation. This insulation is capable of operating at 2400 °F without being damaged. In this system, the amount of material used is dictated by the desired exterior temperature for the vessels (typically 80 °F above ambient); please see the Equipment Specification Sheet for details on the thickness used for this system. The mounting hardware is typically stainless steel.

Inlet Manifold & Outlet Manifolds

All manifolding and sheet metal fabrications are designed per the Sheet Metal and Air Conditioning Contractors' National Association (SMACNA) Standards.

Exhaust Stack

The exhaust stack will be designed by a licensed structural engineer and will accommodate local requirements. The stack will include two sampling ports to accommodate sampling and performance testing. These ports will be in accordance with recommended practice of the EPA.

Diverter Valves

Butterfly type diverter valves as manufactured by Precision Engineered Products (or Equal) are being supplied for this project.

Refer to the Equipment Specification Sheets for specifics concerning these valves.

Oxidizer Fan, Motor, and Variable Frequency Drive

The RTO will require one exhaust fan to move the desired process gas flow through the system. The fan for this system is designed to be induced draft (upstream of the

RTO). The fan is sized to accommodate the pressure drop across the RTO with a negative 1-inWC inlet pressure.

The motor for this fan will be designed to accommodate the necessary power to move the air and will be controlled by a Variable Frequency Drive (V.F.D.). The VFD is used for process flow turndown and is controlled based upon the input from a pressure transmitter located upstream of the RTO fan.

The design basis for the fan/motor/vfd can be found in Equipment Specification Sheets.

Burners and Fuel Trains

The burner(s) provided will be designed to accommodate the heat load necessary to operate the system on a VOC free basis. In this way, the RTO can maintain temperature even when the VOC load has been minimized.

The burner(s) will include a factory assembled, IRI approved gas train, with all required safety features. The fuel to air ratio will be maintained using a mechanically linked position system which will provide "on-ratio" turndown of 16:1 (overall turndown is approximately 50:1).

Standard Control System

A control cabinet will be provided for mounting indoors near the RTO. The cabinet will have 10% open space for future mounting of control equipment and motor controls. The cabinet will be supplied completely pre-wired. As combustion controls and safeties will be hard wired. All wire will be stranded copper with 600-volt insulation type MTW. Minimum size wire will be #16 AWG for control functions and #12 AWG for power functions.

The sub panel will contain a Programmable Logic Controller (PLC), one (1) 7800 Series Honeywell digital flame safeguard flame relay per burner, an inlet pressure transducer for control of the VFD(s), a magnehelic gage, and all necessary relays, terminal strips and fuses to operate the RTO. The panel can be expanded to accommodate additional functions in the future.

The functions for the systems are accessible via Man Machine Interface (MMI). The interface will consist of graphic images that depict the operation of the RTO.

The operator interface also offers access to all P.I.D. analog loop control parameters. The PLC/operator interface will be responsible for handling the following process loops:

1. Maintaining temperature control for each burner.

- 2. Controlling the inlet ductwork pressure.
- 3. Controlling the Gas Injection output (if included).

A microprocessor based Circular Chart Recorder will provide digital indication and continuous printouts of combustion chamber, inlet, and outlet temperature, which can be used for regulatory purposes.

A modem can be included in the control panel for service diagnostics. The modem allows CECO Abatement Systems personnel to monitor and troubleshoot the operation of the RTO remotely.

GAS Injection

CECO Abatement Systems has provided a gas injection system, which offers some operational advantages (i.e. lower gas consumption) but with added risk. The gas consumption using Gas Injection will be as much as 10% less than when operating on burners but because gas is being injected into the inlet manifold, risks of deflagration are increased.

Painting

All mild steel shall receive an SP – 3 finish and will be coated with an industrial epoxy grade painting system.

INSTALLATION DESCRIPTION

CECO Abatement Systems has provided an installation price for the skid mounted option. We have attempted to account for all of the necessary work to get the system installed but the buyer should review the installation scope to insure that all necessary items such as site work, gas piping and electrical power are accounted for.

The mechanical installation of a RTO typically should consist of the following items:

- Unloading and setting the heat recovery chambers/skid on the concrete pad or platform.
- Filling the heat recovery chambers with ceramic recovery media.
- Unloading, setting and fastening the combustion chamber sections.
- Unloading, setting, and fastening the manifolding to the heat recovery chambers.
- Unloading and setting of the RTO process gas fan.

- Unloading, setting, fastening the adjacent ductwork to the RTO fan.
- Assembling the valve actuation system.
- Installation of the burners and associated gas train components.
- Unloading and installation of the exhaust stack.
- Finish/touch-up painting as required after installation is complete.

The electrical installation consists of the following items:

- Setting the control cabinet, VFD in the buyer provided control room.
- Installing the interconnecting wiring between the control cabinet and the skid mounted junction box for skid mounted instruments.
- Installing the interconnecting wiring between the control cabinet and VFD and interconnecting wiring between the motor and VFD assuming that VFD is located within 50 ft of oxidizer motor and adjacent to control panel.

Materials are normally delivered to the site approximately eighteen (18) weeks after CECO ABATEMENT SYSTEMS receives a purchase order. Expedited schedules are often accommodated and are subject to final negotiation.

FIELD SERVICE/ERECTION SUPERVISION

The base bid and optional bid includes two weeks of CECO Abatement Systems field supervision to be used for installation supervision, startup, and training. The proposal does not include standby service. All additional time will be furnished at the per diem rate of \$800 plus travel and living expenses (based on an eight (8) hour work day). Overtime will be billed at 1.5 times our standard rate.

PERFORMANCE GUARANTEES

PERFORMANCE TESTING

All performance guarantees are based on the following criteria:

- 1. Andritz will contract a certified third party to perform the following testing procedures on the equipment:
 - EPA Method 1 and 2 for Volumetric Flow
 - > EPA Method 3 for Oxygen and Carbon Dioxide
 - > EPA Method 4 for Moisture
 - > EPA Method 18 for Organic Compounds
 - > EPA Method 25 for Total Gaseous Non-Methane Organics
 - > EPA Method 25A for Total Hydrocarbon
- 2. The testing will be performed within thirty (30) days of the completion of installation and start-up. All testing will be performed simultaneously on the inlet and outlet of the RTO and the results are reported on a 1-hour time weighted basis. The plant will schedule full production operation for the testing period.

VOLATILE ORGANIC COMPOUNDS (VOCs)

CECO Abatement Systems guarantees that the proposed system will meet 98% destruction of TOTAL hydrocarbons from the customer's process exhaust air-stream at a minimum oxidizer inlet concentration of 300 ppmv as propane. If the inlet concentration is less than 300 ppmv as propane, CECO Abatement Systems will guarantee a maximum exhaust concentration 6 ppmv as propane.

NOx

CECO Abatement Systems guarantees that NOx emissions from the proposed systems, during normal operation, will not exceed 10 ppmv in addition to the NOx concentration measured at the oxidizer inlet. This excludes the NOx contributed via chemical bound nitrogen found in such compounds as amines, ammonia, etc.

EQUIPMENT WARRANTY

CECO Abatement Systems warrants for a period of **five (5)** years from start-up date the following components:

- Internal Insulation
- Oxidizer Housing
- Combustion and Recovery Chambers
- Inlet/Outlet Manifolds
- Fan Inlet/Outlet Ductwork
- Process Exhaust Stack
- Main Diverter Valves (Does not include soft seats, if used)

Should any defect in design, material, workmanship, or operating characteristics develop within the warranty time period, CECO Abatement Systems will replace or correct the component or defect free of charge, subject to the following conditions:

- The purchaser must agree to schedule an RTO inspection with CECO ABATEMENT SYSTEMS annually. The annual estimated cost for this service is shown under "Training/Annual Inspection" below. The purchaser will agree to address any maintenance issues brought to the attention of the purchaser by CECO Abatement Systems inspectors.
- Recommended routine maintenance must be performed and documented per CECO ABATEMENT SYSTEMS instructions at recommended intervals.
- This warranty does not apply to ordinary wear and tear, or deterioration due to corrosives in the process air stream other than those already disclosed to CECO Abatement Systems.

All other items in CECO Abatement Systems scope of supply, including blowers, motors, starters, VFD, fans, burners, etc., are covered by a one (1) year warranty based on CECO ABATEMENT SYSTEMS standard terms and conditions.

HEAT RECOVERY BEDS

CECO Abatement Systems warrants for a period of five (5) years from the date of delivery that the recovery media, when used properly in the normal operations of the RTO, will not cause a significant loss of performance of the system as a result of breakage caused by temperature changes or thermal cycling.

The foregoing warranty shall not cover any failure or damage to the product resulting in whole or in part from any process action or attack of any nature, physical abuse, plugging, improper handling, or operation of the RTO outside of its normal and usual operating parameters or conditions. Furthermore, if monolith media is used, at no time shall the system be operated outside the ranges and thermal design limits of the blocks as specified below:

- > Maximum Heat-Up rate 800 °F per hour over a range from 0 °F to 1800 °F.
- > Maximum cool-down rate 800 °F per hour from 1800 °F to 0 °F.
- > Maximum combustion chamber temperature limit 2000 °F.

Minor damage due to normal wear and tear is excluded from this warranty. Minor thermal cracks that may occur in monolith are normal and do not impair performance - therefore, minor cracking is also excluded. In the event that specific monolithic blocks fail, CECO ABATEMENT SYSTEMS will replace the blocks in question at no additional cost. CECO ABATEMENT SYSTEMS standard terms and conditions apply.

CONDITIONS of PERFORMANCE WARRANTY

CECO Abatement Systems, Inc., guarantees that the proposed RTO system will meet 98% VOC destruction removal efficiency for a period of five (5) years from the date of start-up, subject to the following conditions:

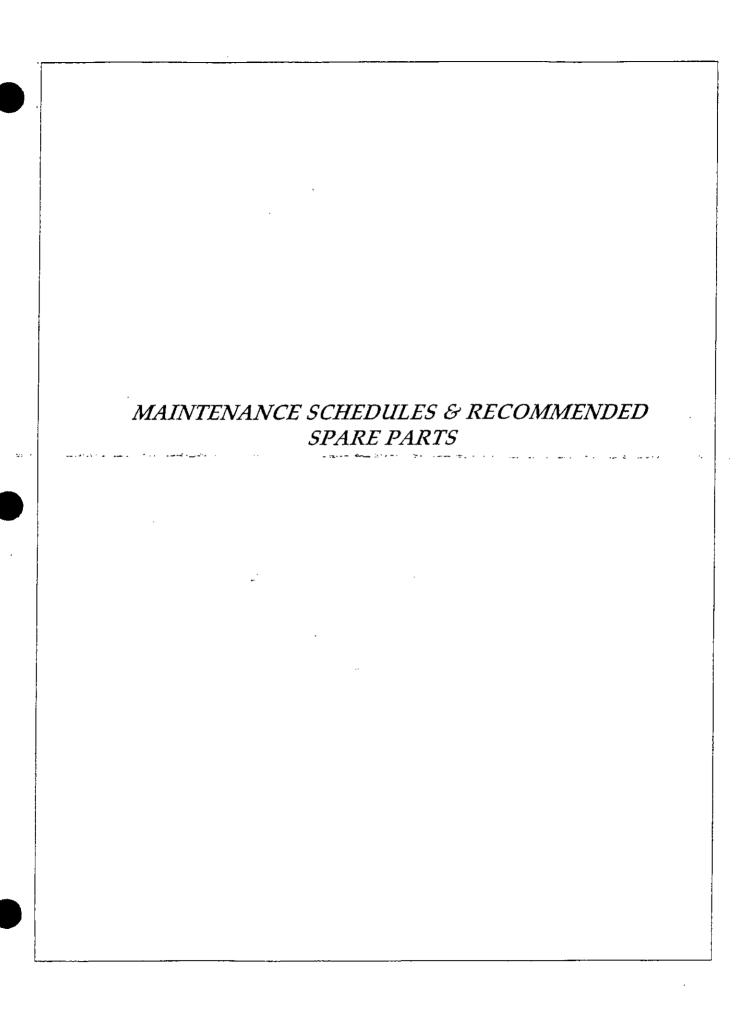
- The purchaser must agree to schedule an RTO inspection with CECO ABATEMENT SYSTEMS annually. The annual estimated cost for this service is shown under "Training/Annual Inspection" below. The purchaser will agree to address any maintenance issues brought to the attention of the purchaser by CECO Abatement Systems inspectors.
- Recommended routine maintenance must be performed and documented per CECO ABATEMENT SYSTEMS instructions at recommended intervals.
- This warranty will become void if the main diverter valves become deteriorated due to the presence of corrosives in the process stream other than those already disclosed to CECO Abatement Systems.

- The inlet process stream constituency does not change significantly from the original design specifications included with this proposal.
- The purchaser will be responsible for all testing and re-testing.

At the end of the warranty period, the purchaser will have the opportunity to extend the performance warranty for an additional period of time at a specific level of performance less than or equal to the current level.

TRAINING/ANNUAL INSPECTION

CECO Abatement Systems Field service can be purchased at the rate of \$800.00 per day plus all reasonable and customary travel and living expenses. A thorough internal and external RTO inspection is estimated to require three days to complete, including travel day each way.



RECOMMENDED MAINTENANCE SCHEDULE

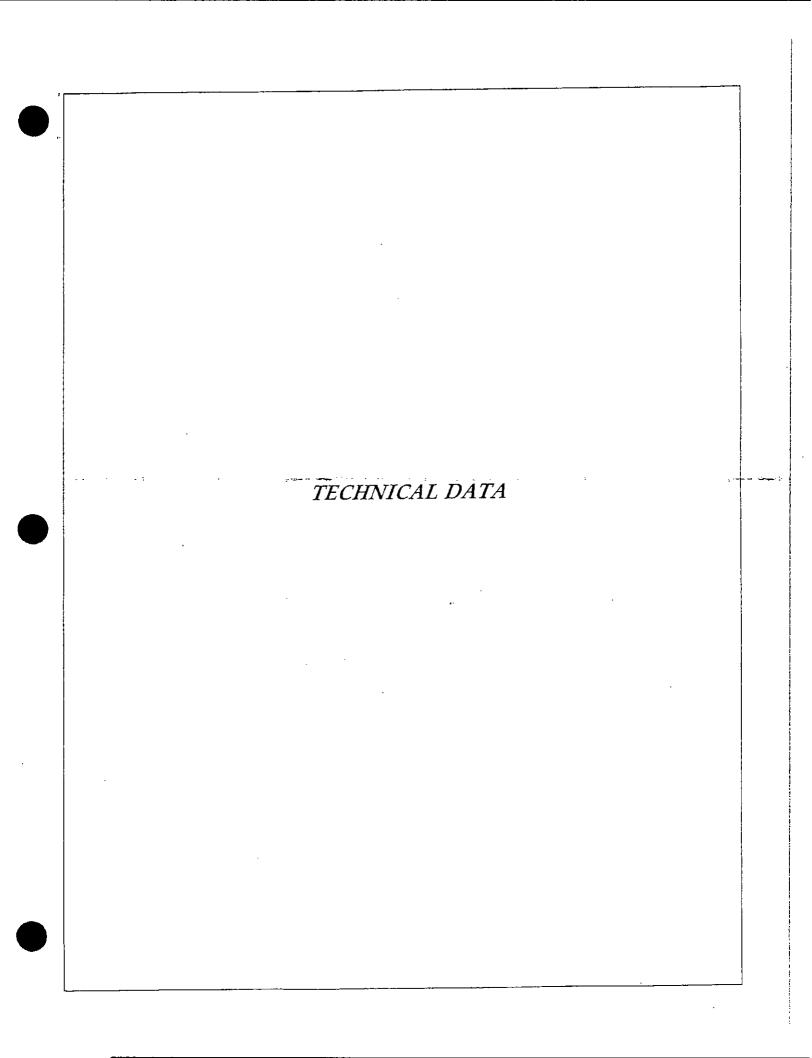
Description	Lubricant		/Κ :	:: MON (1) &	MON5 (4)	: MONS (6)	YR
MAIN DIVERTER VALVE							
Valve Seat Inspection		ì	•			Χ	
Valve Shafts	Anti-Seize					Х	
Valve Shaft Bearings	MobilGrease Special					X	
CHAMBER PURGE VALVES (If	ModuGrease Special						
included)	MobilGrease Special	Ì		1		Х	
Valve Shaft Bearing	MobilGrease Special					χ	
Rod End Bearings	Wiobiioieme opecan	1		<u> </u>			
MECH VALVE DRIVE SYSTEM							-
(IF INCLUDED)	Hub City Synthetic						X
Gear Box	AGMA No. 7; 3 Qts						
Geal box	MobilGrease Special					Х	
Pillow Block Bearings	MobilGrease Special					Х	
Hanger Bearings	Anti-Seize					Х	
Secondary Drive Shafts		ł					
EXHAUST FAN							
External Insulation		1		X			
Wheel & Shaft Inspection		1				х	
Bearing Inspection	<u> </u>			х		1	+
Bearing Lubrication*	Consult Manufacturer			J			
Julia 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2		1		1			
Motor Bearing Lubrication	Consult Manufacturer					X	
PURGE FAN (If included)				<u> </u>			
External Inspection		,	<	} .			
Wheel & Shaft Inspection					•	Х	
Bearing Inspection	 .	- 1	(!	v		
Bearing Lubrication*	Consult Manufacturer			1	Х		
1 A 6 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	C			i		х	
Motor Bearing Lubrication	Consult Manufacturer						
RTO & SYSTEM DAMPERS	M-1-9C Cmanial	1				х	
Pre-Start/Purge Valve Bearings	MobilGrease Special	İ		1 .		x	
Pre-Start/Purge Valve Inspetn.		- [<u> </u>		x	
Recirc. Damper Bearings	MobilGrease Special MobilGrease Special			}		X	i
Inlet Isolatn. Damper Bearings	MobilGrease Special			Ì		x	
Inlet Bypass Damper Bearings	MobilGrease Special	ľ	-	1		X	
Face & Bypass Damper Bearings	MODIFICASE SPECIAL			 			
INSULATION		1		1			x
Inspection				 			
HEAT RECOVERY MEDIA Inspection		j		1			x
MEDIA SUPPORT GRID							
Inspection		{					
nobermu		1		<u> </u>			X
GAS BURNERS							
Discharge Sleeve Inspection				1			х
Spark Ignitor Inspection	l —			1			
BURNER PIPE TRAIN				1		:	34
Gas Shut-off Valves Leak Test							Х
CONTROL INSTRUMENTS				1			
CALIBRATION]		,	
UDC-2000 Controller	_			1			X
UDC-3000 Controller				1			X
UDC-5000 Controller		-		{		j '	X X
Pressure Transmitter	••••					<u> </u>	<u> </u>

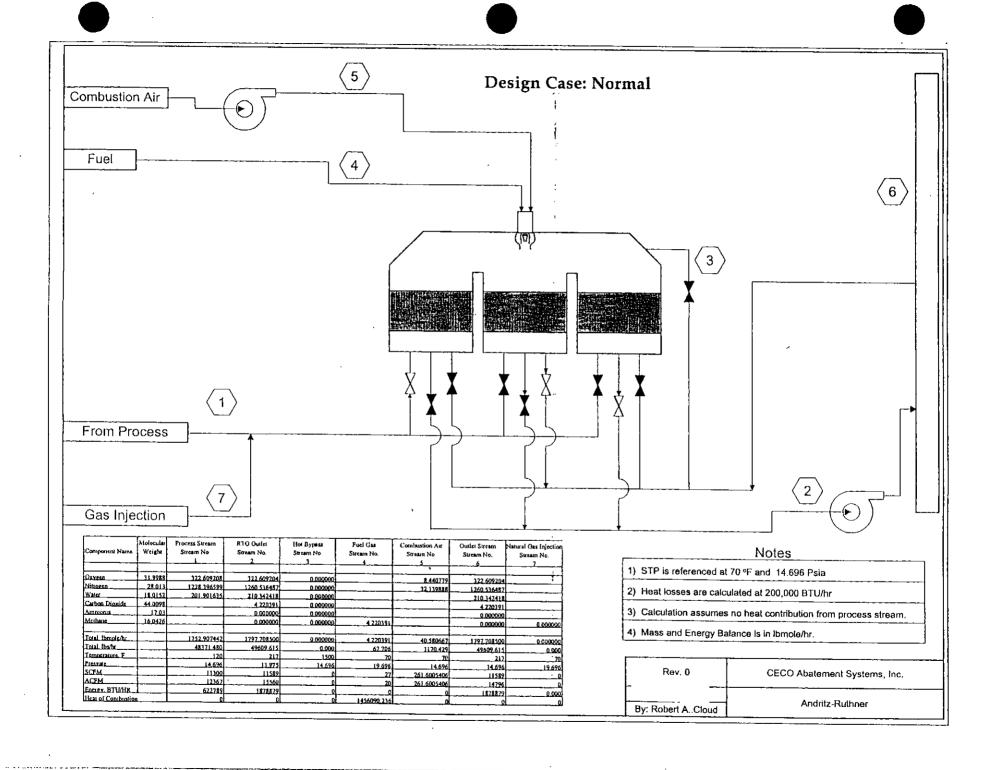
NO-LUBE REQUIRED FOR: Valve Drive DC, Bettis/Bernard Actuators, Honeywell Burner Control Motors, Maxon Safety Shutoff Valves, Combustion Air Blower Motors, Fuel Oil Pump, Air Compressor Motors, Condensate Pump, Condensate Pump Motor

Consult Manufacturer For Lubrication Schedule.

RTO RECOMMENDED SPARE PARTS

OTY	DESCRIPTION
1	Burner Transformers with Cable
2	UV Flame cells
2	Panel Relays
1	Comb. Chamber Thermocouple Assemblies
1	Duct Work Thermocouple Assemblies
1	Flame Guard - PC Controls
 1	Main Fan Motor
1	Combustion Air Fan Motor
1	Pressure/Volume Transducer
1	Analog Input Module
1	Analog Output Module
1	16 Pt Input Module
1	16 Pt Output Module
1	PLC CPU
1	PLC Power Supply
1	Misc. Fuses

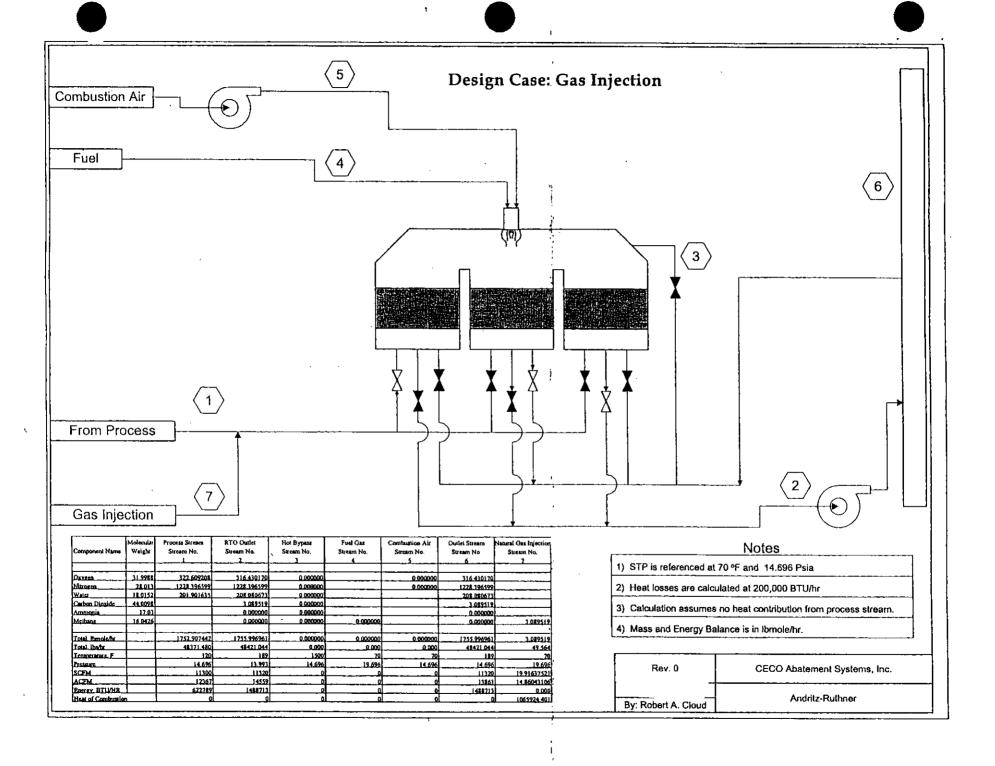




Andritz-Ruthner, Inc.

DESIGN CASE: Normal

		22.1.01.144	
Flow	11300 scfm	Nominal Airflow (SCFM)	11300
Inlet Temperature	120 deg F	Nominal Airflow (ACFM)	12367
Outlet Temperature	216.6 deg F	RTO Inlet Temperature (deg F)	120
Type Of System, Positive or Negative	Negative	RTO Inlet Static Pressure (inWC)	0
Valve Type, Poppet or Butterfly	Butterfly	Process Water Vapor (lb/hr)	3637.30
Fuel Cost	\$ 5.00 \$/MMBTU	Process Dry Gas (lb/hr)	44734.18
Power Cost	\$ 0.05 \$/kWhr	Combustion Chamber Temp (deg F)	1500
Plant Elevation	0 ft ASL	Organic Loading (lb/hr)	0
Local Atmospheric Pressure	14.696 psia	Solvent Gross Heating Value (BTU/lb)	No Solvent Given
Inlet Static Pressure	0 inWC	Fuel Usage (BTU/hr)	1456090
Purge Volume	0 cubic feet	Fuel Cost \$/hr (@, \$ / hr)	7.28
Unit Differential Pressure	-20.0 inWC	RTO Fan BHP Required (Total)	63
DRE	99%	RTO Fan Electrical Usage (kW)	50.79
GAS INJECTION On/Off	OFF	Additional System Power Requirements (kW)	1
Media Bed Depth, ft	7	Total Electrical Usage (kW)	52
Media Type (Monolith/Stoneware)	Monolith	Toral Electrical Cost (@ \$ / hr)	2.6
% XSAir At Burners	15%	Static Pressure @ Design	20.0
Number of Chambers	3	Static Pressure (a) Testblock	22.0
Valve Diameter	26 inches	Fan SCFM @ Testblock	12168
Manifold Diameter	26 inches	Fan ACFM @ Testblock	16338
Combustion Chamber Temp	1500	Gas Molecular Weight	27.60
Heat Losses	200,000 BTU/hr	Fan Inlet Temp	217
Bakeout	OFF	Fan Inlet Density	0.053
Bed Area	33.809524 ft^2	%Bypass	0%
		·	-,-



Andritz-Ruthner, Inc.

DESIGN CASE: Normal

	DESIGN CAS	og: Normal	
Flow	11300 scfm	Nominal Airflow (SCFM)	11300
Inlet Temperature	120 deg F	Nominal Airflow (ACFM)	12367
Outlet Temperature	189.0 deg F	RTO Inlet Temperature (deg F)	120
Type Of System, Positive or Negative	Negative	RTO Inlet Static Pressure (inWC)	0
Valve Type, Poppet or Butterfly	Butterfly	Process Water Vapor (lb/hr)	3637.30
Fuel Cost	\$ 5.00 \$/MMBTU	Process Dry Gas (lb/hr)	44734.18
Power Cost	\$ 0.05 \$/kWhr	Combustion Chamber Temp (deg F)	1500
Plant Elevation	. Oft ASL	Organic Loading (lb/hr)	1300
Local Atmospheric Pressure	14.696 psia	Solvent Gross Heating Value (BTU/lb)	No Salvent Circu
Inlet Static Pressure	0 inWC	Firel Usage (BTU/hr)	No Solvent Given
Purge Volume	0 cubic feet	Fuel Cost \$/hr (@ \$ / hr)	1065924
Unit Differential Pressure	-19.5 inWC	RTO Fan BHP Required (Total)	5.33
DRE	99%	RTO Fan Electrical Usage (kW)	57
GAS INJECTION On/Off	ON	Additional System Power Requirements (kW)	46.30
Media Bed Depth, ft	7	Total Electrical Usage (kW)	46
Media Type (Monolith/Stoneware)	Monolith	Toral Electrical Cost (@ \$ / hr)	46
% XSAir At Burners	15%	Static Pressure @ Design	2.3 19.5
Number of Chambers	3	Static Pressure @ Testblock	
Valve Diameter	26 inches	Fan SCFM @ Testblock	21.5
Manifold Diameter	26 inches	Fan ACFM @ Testblock	11886
Combustion Chamber Temp	1500	Gas Molecular Weight	15287
Heat Losses	200,000 BTU/hr	Fån Inlet Temp	27.57
Bakeout	OFF	Fan Inlet Density	189
Bed Area	33.809524 ft^2	%Bypass	0.055
	001003521112	\4D3 haga	0%

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RTO EXHAUST FAN	cont'd
Motor Bearing RTDs Included?	No
Motor Winding RTDs Included?	Yes
VFD Included?	Yes
VFD Horsepower:	75
VFD Manufacturer:	Allen Bradley or Equal
VFD Type:	Pulse Width Modulated
NEMA Enclosure:	1
BURNER SYSTEM	
Number of Burners:	2
Burner Type:	Nozzle Mix
Burner Manufacturer:	MAXON
Burner Model:	Kinemax
Burner Size:	3"
Burner Fuel:	Natural Gas
Rated Output per Burner:	2 MMBtu/Hr
Over-Fire Capability:	50%
Pilot Output per Burner:	40,000 Btu/Hr.
Number of Fuel Trains:	1
Main/Blocking Valve Manufacturer:	Maxon
Main/Blocking Valve Model No.:	5000 Series
IRI Approved?	Yes
Fuel Train Enclosure Included?	No
Combustion Air Blower Motor Horsepower:	5 HP
Combustion Air Blower Filter/Silencer Included?	Yes
Burner Safeguard Type:	UV Scanner
Burner Access Platform Included?	Yes
Mode of Access:	Ladder
CONTROLS	
	NIENAA 12
Control Panel Enclosure:	NEMA 12 Allen Bradley
PLC Manufacturer: PLC Model:	SLC 504
Human-Machine Interface Manufacturer:	Allen Bradley
Human-Machine Interface Model:	Panelview 1000
Chart Recorder Manufacturer:	Honeywell
Chart Recorder Manufacturer: Chart Recorder Model:	DR450T Truline
Inlet Temp. Recorded?	Yes
Outlet Temp. Recorded?	Yes
Combustion Chamber Temp. Recorded?	Yes
Inlet Pressure/Flow Recorded?	No
Outlet Pressure/Flow Recorded?	No
Flame Safety Manufacturer:	Honeywell
	
Flame Safety Type:	UV-Scanner

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CONTROLS co	nt'd
Control Room Included?	No
Control Room Manufacturer:	N/A
Control Room Size:	N/A
Insulated?	N/A
Air Conditioning?	N/A
Heat?	N/A
Lighting?	N/A
HYDRAULIC SY	STEM
Hydraulic Power Package Included?	No
Hydraulic Pump Manufacturer	N/A
Standby Pump Included?	N/A
Motor Horsepower:	N/A
Reservoir Heater Included?	N/A
Level Alarms Included?	N/A
Nitrogen Charged Accumulator Included?	N/A
PNEUMATIC SY	
Air Compressor Included?	No
Main Regulator Included?	No
Required Supply Pressure:	100 psi
Required Supply Volume:	10 scfm
Nitrogen Charged Accumulator Included?	No
VALVES	
Valve Manufacturer:	PEP or Equal
Main Diverter Valve Diameter:	26 in.
Main Diverter Valve Type:	Butterfly
Main Diverter Valve Valve Seat Style:	Knife-Blade
Mode of Valve Actuation:	Pneumatic
Actuator Manufacturer:	Parker or Equal
Actuation Speed:	1 Sec. Max.
Proximity Switches Included?	Yes
Proximity Switch Manufacturer:	NAMCO or Equal
Pre-Start Purge Valve Included?	Yes
Pre-Start Purge Valve Diameter:	20 in
Pre-Start Purge Valve Type:	Butterfly
Mode of Valve Actuation:	Pneumatic
	Parker or Equal
Actuator Manufacturer:	T direct of Equip
Actuator Manufacturer: Proximity Switches Included?	Yes NAMCO or Equal

VALVES cor	
Vacuum Breaker Included?	Yes
Vacuum Breaker Type:	Valve
Break Pressure:	-10 inWC
Proximity Switches Included?	No
Proximity Switch Manufacturer:	N/A
Chamber Purge Valves Included?	Yes
Chamber Purge Valve Diameter:	14 in.
Chamber Purge Valve Type:	Butterfly
Mode of Valve Actuation:	Pneumatic
Actuator Manufacturer:	Parker
Proximity Switches Included?	Yes
Proximity Switch Manufacturer:	NAMCO or Equal
Bakeout-Cooldown Valve Included?	N/A
Bakeout-Cooldown Valve Diameter:	N/A
Bakeout-Cooldown Valve Type:	N/A
Mode of Valve Actuation:	N/A
Actuator Manufacturer:	N/A
Proximity Switches Included?	N/A
Proximity Switch Manufacturer:	N/A
i loxiliary owners mandacturer.	
Bakeout Re-Circulation Valve Included?	N/A
Bakeout Re-Circulation Valve Diameter:	N/A
Bakeout Re-Circulation Valve Type:	N/A
Mode of Valve Actuation:	N/A
Actuator Manufacturer:	N/A
Proximity Switches Included?	N/A
Proximity Switch Manufacturer:	N/A
Inlet Isolation Valve Included?	Yes
Inlet Isolation Valve Diameter:	26 in
Inlet Isolation Valve Type:	Butterfly
Mode of Valve Actuation:	Pneumatic
Actuator Manufacturer:	Parker or Equal
Proximity Switches Included?	Yes
Proximity Switch Manufacturer:	NAMCO or Equal
Process Dampers Included?	No
Mode of Valve Actuation:	N/A
Actuator Manufacturer:	N/A
Pröximity Switches Included?	N/A
Proximity Switch Manufacturer:	N/A

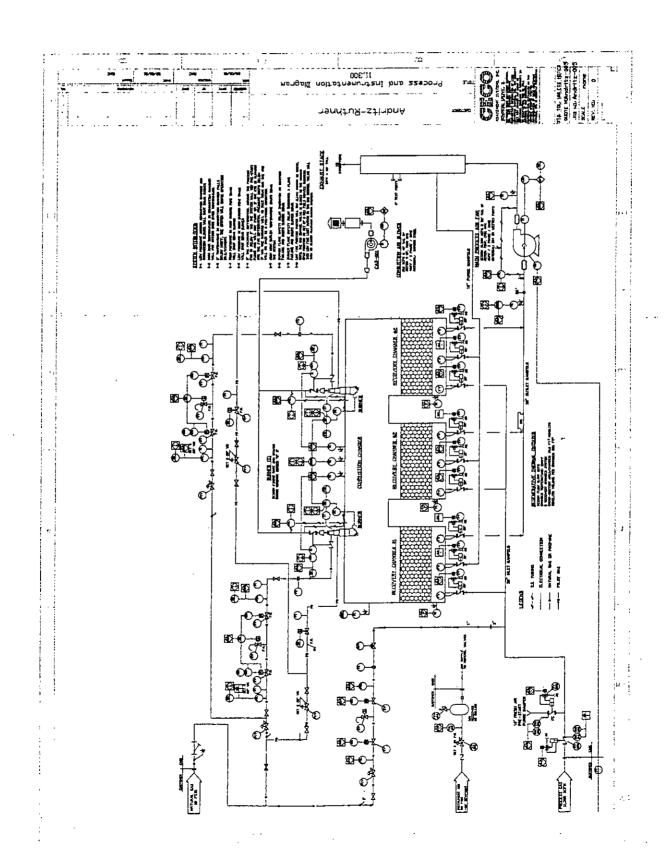
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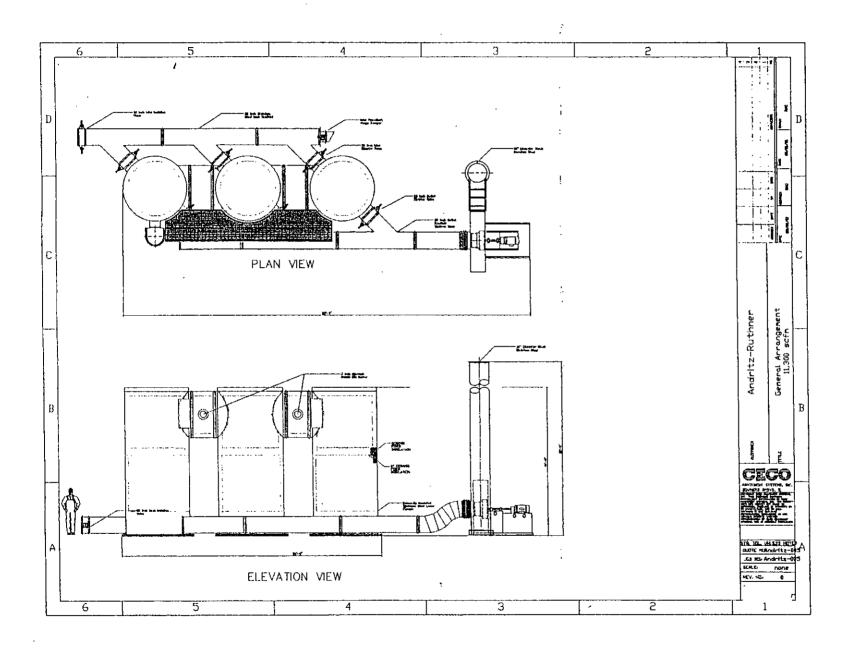
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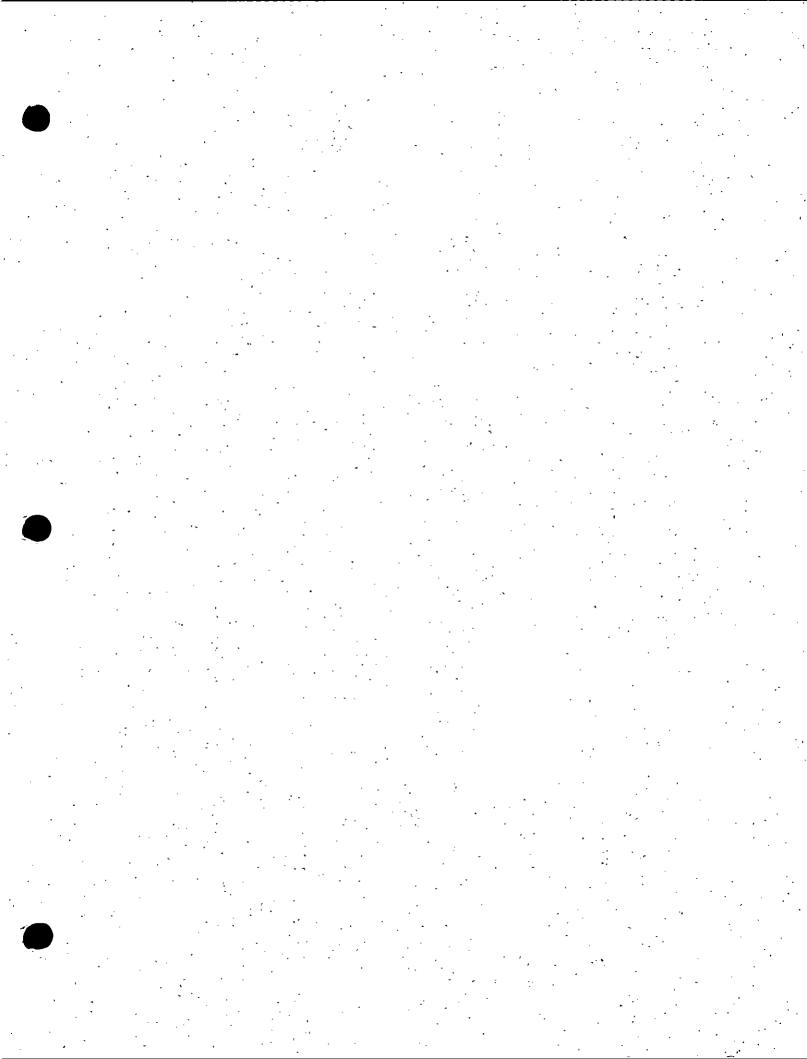
MISCELLANEOUS		
Mechanical Installation Included?	No	
Electrical Installation Included?	No	
Btu-Enhancement (Gas Injection) Included?	Yes	
Foundations Included?	No	
Fire Supression Included?	No	
Exhaust Stack Silencer Included?	N/A	
Skid Mounted	Yes	
Performance Testing Included?	No	

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