

MALCOLM PIRNIE

December 2005 0043-035 Prepared for the

City of Tampa Solid Waste Department



DECEMBER, 2005



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INTRODUCTION

The McKay Bay Refuse-To-Energy Facility (the "Facility") is located in Tampa, Florida and generates electricity from the combustion of approximately 1,000 tons of municipal solid waste per day. The Facility is self-sufficient and operates on a small portion of the electricity it generates. The remaining electricity is sold to the Tampa Electric Company (TECO) and provided to local homes and businesses.

The Facility's major components include four 250 ton per day (nominal) municipal waste combustor (MWC) units with reciprocating grates, a General Electric steam turbine and 22.5 megawatt generator. Each of the four MWC units is equipped with a spray dryer absorber, fabric filter baghouse, a powdered activated carbon injection system, and a selective non-catalytic reduction (SNCR) system.

Facility emissions are currently regulated under permits PSD-FL-086(A) and 0570127-004-AV. Emissions from the four MWC units are monitored by the Continuous Emissions Monitoring System, a complex network of sensors and monitoring equipment that relays emissions data to the Facility operators in the control room. The facility has the following regulated emission sources:

- Four (4) mass-burn municipal waste combustors
- One (1) ash handling system, including scrubbers for ash building and scalper building
- Two (2) lime silos with common vent filter
- Two (2) activated carbon silos, each equipped with a vent filter

The Facility has the following unregulated emissions source:

• One (1) cooling tower

Insignificant emission sources include the following:

- Urea storage tank
- Caustic soda tank
- Sulfuric acid tank
- Boiler chemicals
- Cooling tower chemicals
- Solvent degreaser
- Sandblasting equipment

- Emergency generator
- Diesel fuel storage tank
- Portable air compressors
- Portable welding machines
- Truck traffic
- Fire and safety equipment
- Refuse Pit



Department of Environmental Protection

Division of Air Resource Management APPLICATION FOR AIR PERMIT - LONG FORM

I. APPLICATION INFORMATION

Air Construction Permit - Use this form to apply for an air construction permit for a proposed project:

- subject to prevention of significant deterioration (PSD) review, nonattainment area (NAA) new source review, or maximum achievable control technology (MACT) review; or
- where the applicant proposes to assume a restriction on the potential emissions of one or more pollutants to escape a federal program requirement such as PSD review, NAA new source review, Title V, or MACT; or
- at an existing federally enforceable state air operation permit (FESOP) or Title V permitted facility.

Air Operation Permit – Use this form to apply for:

- an initial federally enforceable state air operation permit (FESOP); or
- an initial/revised/renewal Title V air operation permit.

Air Construction Permit & Revised/Renewal Title V Air Operation Permit (Concurrent Processing Option)

- Use this form to apply for both an air construction permit and a revised or renewal Title V air operation permit incorporating the proposed project.

	To ensure accuracy, please see form instructions.						
<u>Ide</u>	Identification of Facility						
1.	Facility Owner/Company Name: City of Ta	mpa					
2.	Site Name: McKay Bay Refuse-To-Energy	Facility	.				
3.	Facility Identification Number: 0570127						
4.	Facility Location Street Address or Other Locator: 107 North	34 th Street	_				
	City: Tampa County: F	Hillsborough	Zip Code: 33605				
5.	Relocatable Facility? Yes No	6. Existing Title √ Yes	V Permitted Facility?				
Ap	pplication Contact						
1.	Application Contact Name: Christopher C.	Tilman, P.E.					
2.	Application Contact Mailing Address Organization/Firm: Malcolm Pirnie, Inc.						
	Street Address: 4315 Metro Parkway, S	Ste 520					
	City: Fort Myers St	ate: FL	Zip Code: 33916				
3.	Application Contact Telephone Numbers						
	Telephone: (239) 332-1300 ext. Fax: (239) 332-1789						
4. Application Contact Email Address: ctilman@pirnie.com							
Application Processing Information (DEP Use)							
1. Date of Receipt of Application: 12/29/05							
2.	Project Number(s):	05701	27-005-AV				
3.	PSD Number (if applicable):	<u>.</u>					

DEP Form No. 62-210.900(1) - Form

4. Siting Number (if applicable):

Effective: 06/16/03

Purpose of Application	
This application for air permit is submitted to obtain: (Check one)	
Air Construction Permit Air construction permit.	
Air Operation Permit ☐ Initial Title V air operation permit. ☐ Title V air operation permit revision. ☐ Title V air operation permit renewal. ☐ Initial federally enforceable state air operation permit (FESOP) where professional (PE) certification is required. ☐ Initial federally enforceable state air operation permit (FESOP) where professional (PE) certification is not required.	
Air Construction Permit and Revised/Renewal Title V Air Operation Permit (Concurrent Processing) Air construction permit and Title V permit revision, incorporating the proposed proposed program Air construction permit and Title V permit renewal, incorporating the proposed program of the propo	_
Note: By checking one of the above two boxes, you, the applicant, are requesting concurrent processing pursuant to Rule 62-213.405, F.A.C. In such case, you must also check the following box:	,00
☐ I hereby request that the department waive the processing time requirements of the air construction permit to accommodate the processing time frames of the Title V air operation permit.	
Application Comment	
Renewal application for Title V permit no. 0570127-004-AV.	

Effective: 06/16/03

Scope of Application

Description of Emissions Unit	Air Permit Type	Air Permit Proc. Fee
Ash Building and Handling System		
Pebble Lime Storage Silos		
Activated Carbon Storage Silos		
120 MMBtu/hr (max) Municipal Waste Combuster & Auxilary Burners-Unit 1		
120 MMBtu/hr (max) Municipal Waste Combuster & Auxilary Burners-Unit 2		
120 MMBtu/hr (max) Municipal Waste Combuster & Auxilary Burners-Unit 3		
120 MMBtu/hr (max) Municipal Waste Combuster & Auxilary Burners-Unit 4		
Cooling Tower (Unregulated Emissions Unit)		
	Ash Building and Handling System Pebble Lime Storage Silos Activated Carbon Storage Silos 120 MMBtu/hr (max) Municipal Waste Combuster & Auxilary Burners-Unit 1 120 MMBtu/hr (max) Municipal Waste Combuster & Auxilary Burners-Unit 2 120 MMBtu/hr (max) Municipal Waste Combuster & Auxilary Burners-Unit 3 120 MMBtu/hr (max) Municipal Waste Combuster & Auxilary Burners-Unit 4 Cooling Tower	Ash Building and Handling System Pebble Lime Storage Silos Activated Carbon Storage Silos 120 MMBtu/hr (max) Municipal Waste Combuster & Auxilary Burners-Unit 1 120 MMBtu/hr (max) Municipal Waste Combuster & Auxilary Burners-Unit 2 120 MMBtu/hr (max) Municipal Waste Combuster & Auxilary Burners-Unit 3 120 MMBtu/hr (max) Municipal Waste Combuster & Auxilary Burners-Unit 3 120 MMBtu/hr (max) Municipal Waste Combuster & Auxilary Burners-Unit 4 Cooling Tower

Application Processing Fee

Check one: Attached - Amount: \$	\checkmark	Not Applicable
----------------------------------	--------------	----------------

Application Responsible Official Certification

Complete if applying for an initial/revised/renewal Title V permit or concurrent processing of an air construction permit and a revised/renewal Title V permit. If there are multiple responsible officials, the "application responsible official" need not be the "primary responsible official."

1.	Application Responsible Official Name: Stephen W. Daignault, P.E.					
2.	Application Responsible Official Qualification (Check one or more of the following options, as applicable):					
	For a corporation, the president, secretary, treasurer, or vice-president of the corporation in charge of a principal business function, or any other person who performs similar policy or decision-making functions for the corporation, or a duly authorized representative of such person if the representative is responsible for the overall operation of one or more manufacturing, production, or operating facilities applying for or subject to a permit under Chapter 62-213, F.A.C.					
	For a partnership or sole proprietorship, a general partner or the proprietor, respectively. For a municipality, county, state, federal, or other public agency, either a principal executive officer or ranking elected official.					
	The designated representative at an Acid Rain source.					
3.	Organization/Firm: Public Works and Utilities Services					
	City of Tampa					
	Street Address: 306 East Jackson Street, 8N					
	City: Tampa State: FL Zip Code: 33602					
4.	Application Responsible Official Telephone Numbers Telephone: (813) 274-7883 Fax: (813) 274-8127					
5.	Application Responsible Official Email Address: dolores.fernandez@tampagov.net					
6.	Application Responsible Official Certification:					
	I, the undersigned, am a responsible official of the Title V source addressed in this air permit application. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements made in this application are true, accurate and complete and that, to the best of my knowledge, any estimates of emissions reported in this application are based upon reasonable techniques for calculating emissions. The air pollutant emissions units and air pollution control equipment described in this application will be operated and maintained so as to comply with all applicable standards for control of air pollutant emissions found in the statutes of the State of Florida and rules of the Department of Environmental Protection and revisions thereof and all other applicable requirements identified in this application to which the Title V source is subject. I understand that a permit, if granted by the department, cannot be transferred without authorization from the department, and I will promptly notify the department upon sale or legal transfer of the facility or any permitted emissions unit. Finally, I certify that the facility and each emissions unit are in compliance with all applicable requirements to which they are subject, except as identified in compliance plan(s) submitted with this application. Signature Date					

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Professional Engineer Certification

1	Professional Engineer Name: Christopher C. Tilman, P.E.				
1.	Registration Number: 61903				
2	Professional Engineer Mailing Address				
۷.	Organization/Firm: Malcolm Pirnie, Inc.				
	Street Address: 4315 Metro Parkway, Suite 520				
3	City: Fort Myers State: FL Zip Code: 33916 Professional Engineer Telephone Numbers				
٥.					
4.	Telephone: (239) 332-1300 Fax: (239) 332-1789				
	Professional Engineer Email Address: ctilman@pirnie.com Professional Engineer Statement:				
٥.	I, the undersigned, hereby certify, except as particularly noted herein*, that:				
	(1) To the best of my knowledge, there is reasonable assurance that the air pollutant emissions unit(s) and the air pollution control equipment described in this application for air permit, when properly operated and maintained, will comply with all applicable standards for control of air pollutant emissions found in the Florida Statutes and rules of the Department of Environmental Protection; and				
	(2) To the best of my knowledge, any emission estimates reported or relied on in this application are true, accurate, and complete and are either based upon reasonable techniques available for calculating emissions or, for emission estimates of hazardous air pollutants not regulated for an emissions unit addressed in this application, based solely upon the materials, information and calculations submitted with this application.				
	(3) If the purpose of this application is to obtain a Title V air operation permit (check here $\sqrt{}$, if so), I further certify that each emissions unit described in this application for air permit, when properly operated and maintained, will comply with the applicable requirements identified in this application to which the unit is subject, except those emissions units for which a compliance plan and schedule is submitted with this application.				
	(4) If the purpose of this application is to obtain an air construction permit (check here, if so) or concurrently process and obtain an air construction permit and a Title V air operation permit revision or renewal for one or more proposed new or modified emissions units (check here, if so), I further certify that the engineering features of each such emissions unit described in this application have been designed or examined by me or individuals under my direct supervision and found to be in conformity with sound engineering principles applicable to the control of emissions of the air pollutants characterized in this application.				
;	(5) If the purpose of this application is to obtain an initial air operation permit or operation permit revision or renewal for one or more newly constructed or modified emissions units (check here, if so). I further certify that, with the exception of any changes detailed as part of this application, each sich emissions unit has been constructed or modified in substantial accordance with the information given in the corresponding application for air construction permit and with all provisions constructed in substantial accordance with the construction permit.				
	Signature STATE OF 20 202 Signature (Seali) . Corio				

* Attach any exception to certification statement

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II. FACILITY INFORMATION

A. GENERAL FACILITY INFORMATION

Facility Location and Type

1.	1. Facility UTM Coordinates Zone 17 East (km) 360.0 North (km) 3091.9		2.	Facility Latitude/Loc Latitude (DD/MM/ Longitude (DD/MM	SS) 27°56′51"
3.	Governmental	4. Facility Status	5.	Facility Major	6. Facility SIC(s):
	Facility Code:	Code:		Group SIC Code:	4953
	3	Α		49	
7.	Facility Comment:				
	None				·

Facility Contact

1.	Facility Contact Name:		
	Greig Grotecloss, P.E.		
2.	Facility Contact Mailing Address	-	
	Organization/Firm: McKay Bay Refuse	-To-Energy Facility	
	Street Address: 107 North 34th Street	et e	
	City: Tampa	State: FL	Zip Code: 33605
3.	Facility Contact Telephone Numbers:		
	Telephone: (813) 242-5408	Fax: (813) 247-20	052
4.	Facility Contact Email Address: greig.g	rotecloss@ci.tampa.f	1.us

Facility Primary Responsible Official

Complete if an "application responsible official" is identified in Section I. that is not the facility "primary responsible official."

1.	Facility Primary Responsible Official Name:						
2.	Facility Primary Responsible Official Mailing Address Organization/Firm:						
	Street Address:						
	City:		State	e:	7	Zip Code:	
3.	Facility Primary Responsible Official Telephone Numbers						
	Telephone: () - ex	ĸt.	Fax: () -			
4.	Facility Primary Responsible Official Email Address:						

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Facility Regulatory Classifications

Check all that would apply *following* completion of all projects and implementation of all other changes proposed in this application for air permit. Refer to instructions to distinguish between a "major source" and a "synthetic minor source."

1. Small Business Stationary Source Unknown
2. Synthetic Non-Title V Source
3. V Title V Source
4. Major Source of Air Pollutants, Other than Hazardous Air Pollutants (HAPs)
5. Synthetic Minor Source of Air Pollutants, Other than HAPs
6. Major Source of Hazardous Air Pollutants (HAPs)
7. Synthetic Minor Source of HAPs
8. One or More Emissions Units Subject to NSPS (40 CFR Part 60)
9. One or More Emissions Units Subject to Emission Guidelines (40 CFR Part 60)
10. One or More Emissions Units Subject to NESHAP (40 CFR Part 61 or Part 63)
11. Title V Source Solely by EPA Designation (40 CFR 70.3(a)(5))
12. Facility Regulatory Classifications Comment:
Emissions limited by Florida permit no. PSD-FL-086(A).

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List of Pollutants Emitted by Facility

1. Pollutant Emitted	2. Pollutant Classification	3. Emissions Cap [Y or N]?
PM	A	N
SO2	A	Y
NOX	A	Y
СО	A	Y
H106	· A	N
H107	В	N
РВ	В	N
H021	В	N
H114	В	N
DIOX	В	N
H027	В	N

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B. EMISSIONS CAPS

Facility-Wide or Multi-Unit Emissions Caps

1. Pollutant Subject to Emissions Cap	2. Facility Wide Cap [Y or N]? (all units)	3. Emissions Unit ID No.s Under Cap (if not all units)	4. Hourly Cap (lb/hr)	5. Annual Cap (ton/yr)	6. Basis for Emissions Cap
SO ₂	Y			460.0	See 7 below
NO _X	Y			679.0	See 7 below
CO	Y			185.0	See 7 below
_					
	_				
	_				
				,	

7. Facility-Wide or Multi-Unit Emissions Cap Comment:

PSD-FL-086(A) Facility-wide Specific Condition B.8 emissions limits for SO₂, NO_X, and CO.

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C. FACILITY ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1.	Facility Plot Plan: (Required for all permit applications, except Title V air operation
	permit revision applications if this information was submitted to the department within the
	previous five years and would not be altered as a result of the revision being sought)
	Attached, Document ID: Exhibit 1 Previously Submitted, Date:
2.	Process Flow Diagram(s): (Required for all permit applications, except Title V air
	operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being
	sought)
	Attached, Document ID: Exhibit 2 Previously Submitted, Date:
3.	Precautions to Prevent Emissions of Unconfined Particulate Matter: (Required for all
	permit applications, except Title V air operation permit revision applications if this
	information was submitted to the department within the previous five years and would not
	be altered as a result of the revision being sought) Attached Decement ID: Exhibit 2 Decement ID: Exhibit 2
	Attached, Document ID: Exhibit 3 Previously Submitted, Date:
_	Iditional Requirements for Air Construction Permit Applications
1.	Area Map Showing Facility Location:
	Attached, Document ID: Not Applicable (existing permitted facility)
2.	Description of Proposed Construction or Modification:
	Attached, Document ID:
3.	Rule Applicability Analysis:
	Attached, Document ID:
4.	List of Exempt Emissions Units (Rule 62-210.300(3)(a) or (b)1., F.A.C.):
	Attached, Document ID: Not Applicable (no exempt units at facility)
5.	Fugitive Emissions Identification (Rule 62-212.400(2), F.A.C.):
	☐ Attached, Document ID:
6.	Preconstruction Air Quality Monitoring and Analysis (Rule 62-212.400(5)(f), F.A.C.):
	Attached, Document ID: Not Applicable
7.	Ambient Impact Analysis (Rule 62-212.400(5)(d), F.A.C.):
	☐ Attached, Document ID:
8.	Air Quality Impact since 1977 (Rule 62-212.400(5)(h)5., F.A.C.):
	Attached, Document ID:
9.	
	Attached, Document ID: Not Applicable
10	. Alternative Analysis Requirement (Rule 62-212.500(4)(g), F.A.C.):
	☐ Attached, Document ID: ☐ Not Applicable

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Additional Requirements for FESOP Applications 1. List of Exempt Emissions Units (Rule 62-210.300(3)(a) or (b)1., F.A.C.): Attached, Document ID: ✓ Not Applicable (no exempt units at facility) Additional Requirements for Title V Air Operation Permit Applications 1. List of Insignificant Activities (Required for initial/renewal applications only): ✓ Attached, Document ID: Exhibit 4 Not Applicable (revision application) 2. Identification of Applicable Requirements (Required for initial/renewal applications, and for revision applications if this information would be changed as a result of the revision being sought): Attached, Document ID: Exhibit 5 Not Applicable (revision application with no change in applicable requirements) 3. Compliance Report and Plan (Required for all initial/revision/renewal applications): ✓ Attached, Document ID: Exhibit 12 Note: A compliance plan must be submitted for each emissions unit that is not in compliance with all applicable requirements at the time of application and/or at any time during application processing. The department must be notified of any changes in compliance status during application processing. 4. List of Equipment/Activities Regulated under Title VI (If applicable, required for initial/renewal applications only): Attached, Document ID: Equipment/Activities On site but Not Required to be Individually Listed Not Applicable Not 5. Verification of Risk Management Plan Submission to EPA (If applicable, required for initial/renewal applications only): √ Not Applicable Attached, Document ID: 6. Requested Changes to Current Title V Air Operation Permit: Attached, Document ID: Exhibit 7 Not Applicable Additional Requirements Comment

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III. EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Application - For Title V air operation permitting only, emissions units are classified as regulated, unregulated, or insignificant. If this is an application for Title V air operation permit, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each regulated and unregulated emissions unit addressed in this application for air permit. Some of the subsections comprising the Emissions Unit Information Section of the form are optional for unregulated emissions units. Each such subsection is appropriately marked. Insignificant emissions units are required to be listed at Section II, Subsection C.

Air Construction Permit or FESOP Application - For air construction permitting or federally enforceable state air operation permitting, emissions units are classified as either subject to air permitting or exempt from air permitting. The concept of an "unregulated emissions unit" does not apply. If this is an application for air construction permit or FESOP, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air permitting are required to be listed at Section II, Subsection C.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit Application – Where this application is used to apply for both an air construction permit and a revised/renewal Title V air operation permit, each emissions unit is classified as either subject to air permitting or exempt from air permitting for air construction permitting purposes and as regulated, unregulated, or insignificant for Title V air operation permitting purposes. The air construction permitting classification must be used to complete the Emissions Unit Information Section of this application for air permit. A separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air construction permitting and insignificant emissions units are required to be listed at Section II, Subsection C.

If submitting the application form in hard copy, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application must be indicated in the space provided at the top of each page.

A. GENERAL EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Emissions Unit Classification

1.	Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)								
	emissions t	ınit.					Init Information S Init Information S		
			issions unit.	m u	115 E11115510	115 C	onit information 5	ccu	On is an
En	nissions Unit	Des	cription and Sta	tus			-		
1.	Type of Emis	ssio	ns Unit Addresse	d in	this Sectio	n: (Check one)		
	process o	r pro		acti	vity, which	pro	es, as a single em duces one or more stack or vent).		_
	process o	r pro		d ac	ctivities whi	ich l	nas at least one de		ons unit, a group of ble emission point
							ses, as a single em which produce fug		
2.	Description of	of E	missions Unit Ad	ldre	ssed in this	Sec	tion:		
	Ash Handling	g Sy	stem, including	scru	bbers for as	sh b	uilding and scalpe	r bu	ilding
3.	Emissions U	nit I	dentification Nur	nbe	r: 100				
4.	Emissions	5.	Commence	6.	Initial	7.		8.	
	Unit Status Code:		Construction Date:		Startup Date:		Major Group SIC Code:		Yes
	A		Date.		08/30/01		49		√ No
9.	Package Unit	L t:		<u>L</u>					
	Manufacture		ri-Mer Corp.			Мо	del Number:		
10	10. Generator Nameplate Rating: N/A								
11	11. Emissions Unit Comment:								

Emissions Unit Control Equipment

1.	Control Equipment/Method(s) Description:
	This emissions unit uses two wet scrubbers and a containment building to control fugitive emissions.
2.	Control Device or Method Code(s): 141, 54
<u> </u>	

B. EMISSIONS UNIT CAPACITY INFORMATION

(Optional for unregulated emissions units.)

Emissions Unit Operating Capacity and Schedule

1.	Maximum Process or Throughput Rate: 280 tons/day (see note 6)						
2.	Maximum Production Rate:						
3.	Maximum Heat Input Rate:						
4.	Maximum Incineration Rate:						
5.	Requested Maximum Operat	ing Schedule:					
		24 hours/day	7 days/week				
		52 weeks/year	8,760 hours/year				
6.	Operating Capacity/Schedule	Comment:					
	280 tons/day maximum proceonly, and is not a compliance	ess/throughput rate is provided requirement.	l for informational purposes				

C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

Emission Point Description and Type

1.	Identification of Point on I Flow Diagram: See Exhib		2. Emission Point	Гуре Code: 3		
3.	Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking:					
	Ash handling system scrub	ober stacks				
		·				
4.	ID Numbers or Description	ns of Emission Ur	nits with this Emission	n Point in Common:		
	Not Applicable					
5.	Discharge Type Code: V	6. Stack Height 50 feet	:	7. Exit Diameter: 1.3 feet		
8.	Exit Temperature: N/A	9. Actual Volum	metric Flow Rate:	10. Water Vapor: N/A		
11.	. Maximum Dry Standard F	low Rate:	12. Nonstack Emiss	ion Point Height:		
13.	Emission Point UTM Coo Zone: 17 East (km):	rdinates	14. Emission Point Latitude/Longitude Latitude (DD/MM/SS)			
	North (km)	:	Longitude (DD/	MM/SS)		
15.	Emission Point Comment:					

D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment Description and Rate: Segment $\underline{1}$ of $\underline{2}$

1. Se	1. Segment Description (Process/Fuel Type):						
Inc	Industrial Processes – Mineral Processes						
	Bulk Materials Conve		Classified				
2. Sc	ource Classification Code	e (SCC):	3. SCC Units:				
30	510199		Tons Transi	ferred	or Handled		
4. M	aximum Hourly Rate:	5. Maximum	Annual Rate:		Estimated Annual Activity Factor:		
1	aximum % Sulfur:	8. Maximum	% Ash:		Million Btu per SCC Unit:		
N/		N/A]	N/A		
10. Se	egment Comment:						
<u>Segm</u>	ent Description and Ra	te: Segment 2 o	of <u>2</u>				
1. Se	egment Description (Proc	ess/Fuel Type):					
2. Sc	ource Classification Code	e (SCC):	3. SCC Units:				
4. M	aximum Hourly Rate:	5. Maximum	Annual Rate:	6.]	Estimated Annual Activity		
	-			l	Factor:		

7. Maximum % Sulfur:

10. Segment Comment:

8. Maximum % Ash:

9. Million Btu per SCC Unit:

E. EMISSIONS UNIT POLLUTANTS

List of Pollutants Emitted by Emissions Unit

1. Pollutant Emitted	2. Primary Control	3. Secondary Control	4. Pollutant
	Device Code	Device Code	Regulatory Code
VE (Opacity)	141	054	EL
	_		_
		_	_

G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

<u>Visible Emissions Limitation:</u> Visible Emissions Limitation $\underline{1}$ of $\underline{1}$

1.	Visible Emissions Subtype: VE05	2. Basis for Allowable Opacity: √ Rule ☐ Other
3.	Allowable Opacity: Normal Conditions: 5 % Ex Maximum Period of Excess Opacity Allower	acceptional Conditions: 100 % ed: 2 hours
4.	Method of Compliance: Compliance with opacity emission limits with Reference Method 22.	ill be demonstrated annually using EPA
5.		o, shut-down or malfunction, provided that the sions are adhered to and the duration of these our period (Rule 62-210.700(1), F.A.C.).
<u>Vi</u>	sible Emissions Limitation: Visible Emissi	ons Limitation of
1.	Visible Emissions Subtype:	2. Basis for Allowable Opacity: Rule Other
3.	Allowable Opacity: Normal Conditions: % Ex Maximum Period of Excess Opacity Allow	acceptional Conditions: % ed: min/hour
4.	Method of Compliance:	
5.	Visible Emissions Comment:	

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 2 Previously Submitted, Date
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 8 Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 9 Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Value Previously Submitted, Date Previously Submitted, Date Not Applicable (construction application)
5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Value Previously Submitted, Date Previously Submit
6.	Compliance Demonstration Reports/Records Attached, Document ID: Test Date(s)/Pollutant(s) Tested:
	Previously Submitted, Date: November 18, 2005 Test Date(s)/Pollutant(s) Tested: 2005 compliance testing results and 2004 Statement of Compliance are included in Exhibit 12. □ To be Submitted, Date (if known): Test Date(s)/Pollutant(s) Tested:
-	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute Attached, Document ID:

Additional Requirements for Air Construction Permit Applications

1. Control Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7),	
F.A.C.; 40 CFR 63.43(d) and (e)) ☐ Attached, Document ID:	
2. Good Engineering Practice Stack Height Analysis (Rule 62-212.400(5)(h)6., F.A.C.,	and
2. Good Engineering Fractice Stack Height Analysis (Rule 62-212.400(3)(11)6., F.A.C., Rule 62-212.500(4)(f), F.A.C.)	anu
Attached, Document ID: \(\sqrt{Not Applicable} \)	
3. Description of Stack Sampling Facilities (Required for proposed new stack sampling	
facilities only)	
Attached, Document ID:	
Additional Requirements for Title V Air Operation Permit Applications	
 Identification of Applicable Requirements ✓ Attached, Document ID: Exhibit 5 	
2. Compliance Assurance Monitoring	
3. Alternative Methods of Operation ☐ Attached, Document ID:	
4. Alternative Modes of Operation (Emissions Trading)	
Attached, Document ID: \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \	
5. Acid Rain Part Application	
Certificate of Representation (EPA Form No. 7610-1)	
Copy Attached, Document ID:	
Acid Rain Part (Form No. 62-210.900(1)(a))	
Attached, Document ID:	
Previously Submitted, Date:	
Repowering Extension Plan (Form No. 62-210.900(1)(a)1.) Attached, Document ID:	
Previously Submitted, Date:	
New Unit Exemption (Form No. 62-210.900(1)(a)2.)	
Attached, Document ID:	
Previously Submitted, Date:	
Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)	
Attached, Document ID:	
Previously Submitted, Date:	
Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)	
Attached, Document ID:	
Previously Submitted, Date:	
Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)	
Attached, Document ID:	
Previously Submitted, Date:	
Vot Applicable	

Additional Requirements Comment		
None		

A. GENERAL EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Emissions Unit Classification

1.	Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)								
	 ✓ The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit. ☐ The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit. 								
<u>En</u>	nissions Unit	<u>Des</u>	cription and Sta	tus	<u>i</u>				
1.	Type of Emis	ssio	ns Unit Addresse	d ir	this Sectio	n: (Check one)		
	process o which ha	r pros	oduction unit, or least one definab	act le e	ivity, which emission poi	pro int (e ai	r pollutants and
	process o	r pr		ıd a	ctivities wh	ich	has at least one de		ons unit, a group of able emission point
							ses, as a single em hich produce fug		
2.	. Description of Emissions Unit Addressed in this Section:								
	Pebble Lime	Sto	rage Silos						
3.	Emissions U	nit I	dentification Nui	mbe	er: 101				
4.	Emissions	5.	Commence	6.	Initial	7.		8.	Acid Rain Unit?
	Unit Status		Construction		Startup		Major Group SIC Code:		Yes
	Code:		Date:		Date: 08/30/01		49		√ No
9.	Package Uni	t:							
	Manufacture					Мо	del Number: Seri	al N	lo.
10	. Generator N	lamo	eplate Rating: N	I/A					
11	. Emissions U	nit (Comment:						
	Two (2) silos with common vent filter for storage of pebble lime used for acid gas control in SDA units.								

Emissions Unit Control Equipment

1. Control Equipment/Method(s) Description:
This emissions unit is equipped with a fabric filter on the silo exhaust that activates only during silo loading operations.
2. Control Device or Method Code(s): 18

B. EMISSIONS UNIT CAPACITY INFORMATION

(Optional for unregulated emissions units.)

Emissions Unit Operating Capacity and Schedule

1.	Maximum Process or Throughput Rate: 3,300 tons/year	
2.	Maximum Production Rate:	
3.	Maximum Heat Input Rate:	
4.	Maximum Incineration Rate:	
5.	Requested Maximum Operating Schedule:	
	hours/day	days/week
	weeks/year	500 hours/year

6. Operating Capacity/Schedule Comment:

The vent filter serving the lime silos only activates (exhausts carrier air) during lime loading operations, which occur approximately 500 hours per year. The silos continuously feed lime to the slakers that serve the SDA units.

C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

Emission Point Description and Type

1.	Identification of Point on Plot Plan or Flow Diagram: See Exhibit 1		2. Emission Point	Гуре Code: 2		
3.	Descriptions of Emission		this Emissions Unit	for VE Tracking:		
	Not Applicable					
4.	ID Numbers or Description	ns of Emission Ur	nits with this Emission	n Point in Common:		
	Not Applicable					
5.	Discharge Type Code: P	6. Stack Height	:	7. Exit Diameter:		
8.	Exit Temperature: Ambient	9. Actual Volum	metric Flow Rate:	10. Water Vapor:		
11	. Maximum Dry Standard F 1,200 dscfm	Flow Rate:	12. Nonstack Emission Point Height:			
13	Emission Point UTM Coo Zone: 17 East (km):	rdinates	14. Emission Point Latitude/Longitude Latitude (DD/MM/SS)			
	North (km)		Longitude (DD/	MM/SS)		
15	15. Emission Point Comment: Two pebble lime storage silos exhaust through a common vent filter during silo loading operations.					
	•					

E. EMISSIONS UNIT POLLUTANTS

List of Pollutants Emitted by Emissions Unit

1. Pollutant Emitted	Primary Control Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
PM	018		EL

POLLUTANT DETAIL INFORMATION Page [1] of [1]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted: PM	2. Total Pero	cent Efficiency of Control:
3.	Potential Emissions:		4. Synthetically Limited?
	0.36 lb/hour	tons/year	☐ Yes ✓ No
5.	Range of Estimated Fugitive Emissions (as	applicable):	
6.	Emission Factor: 0.015 grains/dscf	•	7. Emissions
	Reference: PSD-FL-086(A)		Method Code: 5
8.	Calculation of Emissions:		•
	Limited by Florida permit PSD-FL-086(A)		
9.	Pollutant Potential/Estimated Fugitive Emis	sions Commen	nt:
	Limited by Florida permit PSD-FL-086(A)		

POLLUTANT DETAIL INFORMATION Page [1] of [1]

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions $\underline{1}$ of $\underline{11}$

Basis for Allowable Emissions Code: RULE	2. Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units: 0.015 grains/dscf	4. Equivalent Allowable Emissions: 0.36 lb/hour tons/year		
5. Method of Compliance: This emissions unit has the potential to emi baghouse.	This emissions unit has the potential to emit less than 100 tons per year and is equipped with a		
6. Allowable Emissions Comment (Description of Operating Method): Limited by Florida permit PSD-FL-086(A)			
Allowable Emissions 2 of 11			

1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Emissions:	of Allowable
3.	Allowable Emissions and Units:	4.	Equivalent Allowable I	Emissions:
	1		lb/hour	tons/year
5.	Method of Compliance:			
6.	Allowable Emissions Comment (Description of C)ner	ating Method):	
	Anowable Limssions Comment (Description of \	Sper	ating Method).	
	Anomable Emissions Comment (Description of V	Oper	ating Method).	
	Anowable Emissions Comment (Description of v	Эрсг	ating Method).	

Allowable Emissions 3 of 11

		_	
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:		
6.	Allowable Emissions Comment (Description of Comment)	Oper	ating Method):

G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

<u>Visible Emissions Limitation:</u> Visible Emissions Limitation $\underline{1}$ of $\underline{1}$

1.	Visible Emissions Subtype: VE05	 Basis for Allowable Op	acity:] Other
3.	1 3	ceptional Conditions:	100 % 2 hours
4.	Method of Compliance: EPA Method 9 shall be used to determine op F.A.C.	acity compliance pursuant t	o Chapter 62-297,
5.	Visible Emissions Comment: Excess emissions are allowed during startup, operational practices are adhered to and the chours in any 24-hour period (Rule 62-210.70)	duration of these events does	~
<u>Vi</u>	sible Emissions Limitation: Visible Emission	ons Limitation of	
1.	Visible Emissions Subtype:	2. Basis for Allowable Op Rule	acity: Other
3.	Allowable Opacity: Normal Conditions: % Exc Maximum Period of Excess Opacity Allower	ceptional Conditions: d:	% min/hour
4.	Method of Compliance:		
5.	Visible Emissions Comment:		

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1	. Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)
2	
3	. Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 9 Previously Submitted, Date
4	Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 10 Previously Submitted, Date
5	 Not Applicable (construction application) Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)
6	Compliance Demonstration Reports/Records Attached, Document ID: Test Date(s)/Pollutant(s) Tested:
	✓ Previously Submitted, Date: November 18, 2005 Test Date(s)/Pollutant(s) Tested: 2005 compliance testing results and 2004 Statement of Compliance are included in Exhibit 12. To be Submitted, Date (if known): Test Date(s)/Pollutant(s) Tested:
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7	 Other Information Required by Rule or Statute ☐ Attached, Document ID:

Additional Requirements for Air Construction Permit Applications

1.	Control Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7), F.A.C.; 40 CFR 63.43(d) and (e))
	Attached, Document ID: \[\sqrt{Not Applicable} \]
2.	Good Engineering Practice Stack Height Analysis (Rule 62-212.400(5)(h)6., F.A.C., and
	Rule 62-212.500(4)(f), F.A.C.)
	Attached, Document ID:
3.	Description of Stack Sampling Facilities (Required for proposed new stack sampling facilities only)
	Attached, Document ID: Not Applicable
Ac	Iditional Requirements for Title V Air Operation Permit Applications
1.	Identification of Applicable Requirements
	√ Attached, Document ID: Exhibit 5
2.	Compliance Assurance Monitoring
	Attached, Document ID: Exhibit 6 Not Applicable
3.	Alternative Methods of Operation
	Attached, Document ID: Not Applicable
4.	Alternative Modes of Operation (Emissions Trading)
	Attached, Document ID: Not Applicable
5.	Acid Rain Part Application
	Certificate of Representation (EPA Form No. 7610-1)
	Copy Attached, Document ID:
	Acid Rain Part (Form No. 62-210.900(1)(a))
	Attached, Document ID:
	Previously Submitted, Date:
	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
	Attached, Document ID:
	Previously Submitted, Date: New Unit Exemption (Form No. 62-210.900(1)(a)2.)
	Attached, Document ID:
	Previously Submitted, Date:
	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)
	Attached, Document ID:
	Previously Submitted, Date:
	Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)
	Attached, Document ID:
	Previously Submitted, Date:
	Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)
	Attached, Document ID:
	Previously Submitted, Date:
	√ Not Applicable

EMISSIONS UNIT INFORMATION Section [2] of [8] Additional Requirements Comment None

A. GENERAL EMISSIONS UNIT INFORMATION

<u>Title V Air Operation Permit Emissions Unit Classification</u>

1.	Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)								
	 ✓ The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit. ☐ The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit. 								
En	nissions Unit	Des	cription and Sta	tus					
1.	Type of Emis	ssio	ns Unit Addresse	d in	this Sectio	n:	(Check one)		
	process o	r pr		acti	vity, which	pro	ses, as a single emoduces one or morestack or vent).		_
	process o	r pr		d a	ctivities wh	ich	has at least one de		ons unit, a group of ole emission point
							ses, as a single em which produce fug		
2.	2. Description of Emissions Unit Addressed in this Section:								
	Activated Ca	ırboı	n Storage Silos						
3.	Emissions U	nit I	dentification Nui	mbe	er: 102				
4.	Emissions	5.	Commence	6.	Initial	7.	Emissions Unit	8.	Acid Rain Unit?
	Unit Status		Construction		Startup		Major Group		Yes
	Code:		Date:		Date:		SIC Code:		√ No
	A				08/30/01		49		
9.	Package Unit Manufacture					Ma	del Number: Seri	-1 NL	•
10			eplate Rating: N	I/A		IVIC	dei Nuiliber: Seit	ai iv	0.
				1/11					
11	11. Emissions Unit Comment: Two (2) activated carbon storage silos used for mercury control in SDA units. Each silo is equipped with a vent filter that operates only during silo loading operations.								

Emissions Unit Control Equipment

1.	Control Equipment/Method(s) Description:
	This emissions unit is equipped with a fabric filter on each silo exhaust that activates only during silo loading operations.
	·
2.	Control Device or Method Code(s): 18

B. EMISSIONS UNIT CAPACITY INFORMATION

(Optional for unregulated emissions units.)

Emissions Unit Operating Capacity and Schedule

1.	. Maximum Process or Throughput Rate: 120 tons/year						
2.	Maximum Production Rate:						
3.	Maximum Heat Input Rate:						
4.	Maximum Incineration Rate:						
5.	Requested Maximum Operating Schedule:						
	hours/day	days/week					
	weeks/year	100 hours/year					
6.	Operating Capacity/Schedule Comment:						
	The vent filters serving the carbon silos only activate (exhaust carrier air) during carbon loading operations, which occur approximately 100 hours per year. The silos continuously feed activated carbon to the SDA units.						

C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

Emission Point Description and Type

1.	Identification of Point on Flow Diagram: See Exhib		2. Emission Point 7	Type Code: 2		
3.	Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking:					
	Not Applicable					
_			 			
4. 	ID Numbers or Description	ons of Emission Ur	nits with this Emission	n Point in Common:		
	Not Applicable					
5.	Discharge Type Code: P	6. Stack Height	•	7. Exit Diameter:		
8.	Exit Temperature: Ambient	9. Actual Volum	netric Flow Rate:	10. Water Vapor:		
11	. Maximum Dry Standard I 1,200 dscfm	Flow Rate:	12. Nonstack Emission Point Height:			
13	Emission Point UTM Coc Zone: 17 East (km):	ordinates	14. Emission Point Latitude/Longitude Latitude (DD/MM/SS)			
	North (km)):	Longitude (DD/I	MM/SS)		
15	North (km): Longitude (DD/MM/SS) 15. Emission Point Comment: Each activated carbon storage silo exhausts through a vent filter during silo loading operations.					

E. EMISSIONS UNIT POLLUTANTS

List of Pollutants Emitted by Emissions Unit

1. Pollutant Emitted	Primary Control Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
PM	018		EL
			_

POLLUTANT DETAIL INFORMATION
Page [1] of [1]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: PM	2. Total Percent Efficiency of Control:			
3.	Potential Emissions:				cally Limited?
	0.36 lb/hour	tons/year	🗆 Y	es	√ No
5.	Range of Estimated Fugitive Emissions (as	applicable):			
6.	Emission Factor: 0.015 grains/dscf			7.	Emissions
	Reference: PSD-FL-086(A)				Method Code:
					5
8.	Calculation of Emissions:				
	Limited by Florida permit PSD-FL-086(A)				
9.	Pollutant Potential/Estimated Fugitive Emis	sions Commen	t:		
	Limited by Florida permit PSD-FL-086(A)				

POLLUTANT DETAIL INFORMATION Page [1] of [1]

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 1 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:				
3.	Allowable Emissions and Units: 0.015 grains/dscf	4. Equivalent Allowable Emissions: 0.36 lb/hour tons/year					
5.	Method of Compliance: This emissions unit has the potential to emit less than 100 tons per year and is equipped with a baghouse.						
6.	6. Allowable Emissions Comment (Description of Operating Method): Limited by Florida permit PSD-FL-086(A)						
<u>Al</u>	lowable Emissions Allowable Emissions 2 o	f <u>11</u>					
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:				
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour				
6.	5. Method of Compliance:6. Allowable Emissions Comment (Description of Operating Method):						
Al	lowable Emissions Allowable Emissions 3 o	f <u>11</u>					
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:				
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year				
5.	Method of Compliance:						
6.	Allowable Emissions Comment (Description of	Opei	ating Method):				

G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

Visible Emissions Limitation: Visible Emissions Limitation 1 of 1

1.	Visible Emissions Subtype: VE05	2. Basis for Allowable Opacity: √ Rule
	<u> </u>	Nuic Guier
3.	Allowable Opacity: Normal Conditions: 5% Ex Maximum Period of Excess Opacity Allower	acceptional Conditions: 100 % ed: 2 hours
4.	Method of Compliance: EPA Method 9 shall be used to determine of F.A.C.	pacity compliance pursuant to Chapter 62-297,
5.	Visible Emissions Comment: Excess emissions are allowed during startup operational practices are adhered to and the hours in any 24-hour period (Rule 62-210.7	
Vi	sible Emissions Limitation: Visible Emissi	ons Limitation of
1.	Visible Emissions Subtype:	2. Basis for Allowable Opacity: Rule Other
3.	Allowable Opacity: Normal Conditions: % Ex Maximum Period of Excess Opacity Allower	acceptional Conditions: % ed: min/hour
4.	Method of Compliance:	
5.	Visible Emissions Comment:	

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

	1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 2 Previously Submitted, Date
	2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 8 Previously Submitted, Date
		Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 9 Previously Submitted, Date
	4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) V Attached, Document ID: Exhibit 10
	5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 11 Previously Submitted, Date Not Applicable
	6.	Compliance Demonstration Reports/Records Attached, Document ID: Test Date(s)/Pollutant(s) Tested:
		✓ Previously Submitted, Date: November 18, 2005 Test Date(s)/Pollutant(s) Tested: 2005 compliance testing results and 2004 Statement of Compliance are included in Exhibit 12. To be Submitted, Date (if known): Test Date(s)/Pollutant(s) Tested:
1		Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
	7.	Other Information Required by Rule or Statute Attached, Document ID: Not Applicable

EMISSIONS UNIT INFORMATION

Section [3] of [8]

Additional Requirements for Air Construction Permit Applications

1.	Control Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7),
ļ	F.A.C.; 40 CFR 63.43(d) and (e)) ☐ Attached, Document ID:
<u> </u>	<u> </u>
2.	Good Engineering Practice Stack Height Analysis (Rule 62-212.400(5)(h)6., F.A.C., and Rule 62-212.500(4)(f), F.A.C.)
	☐ Attached, Document ID:
3.	
]	facilities only)
	Attached, Document ID: Not Applicable
<u>A</u> (dditional Requirements for Title V Air Operation Permit Applications
1.	Identification of Applicable Requirements
	√ Attached, Document ID: Exhibit 5
$\frac{1}{2}$	Compliance Assurance Monitoring
	Attached, Document ID: Exhibit 6 Not Applicable
3	Alternative Methods of Operation
]	☐ Attached, Document ID:
_	
4.	Alternative Modes of Operation (Emissions Trading)
	☐ Attached, Document ID: Not Applicable
5.	Acid Rain Part Application
	Certificate of Representation (EPA Form No. 7610-1)
	Copy Attached, Document ID:
	☐ Acid Rain Part (Form No. 62-210.900(1)(a))
1	Attached, Document ID:
	Previously Submitted, Date:
	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
	Attached, Document ID:
	Previously Submitted, Date:
	New Unit Exemption (Form No. 62-210.900(1)(a)2.)
	Attached, Document ID:
	Previously Submitted, Date:
	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)
	Attached, Document ID:
	Previously Submitted, Date:
	☐ Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)
	Attached, Document ID:
	Previously Submitted, Date:
	Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)
	Attached, Document ID:
	Previously Submitted, Date:
	√ Not Applicable

EMISSIONS UNIT INFORMATION Section [3] of [8] Additional Requirements Comment None

None		-

A. GENERAL EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Emissions Unit Classification

1.	1. Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)							
	 ✓ The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit. ☐ The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit. 							
<u>En</u>	nissions Unit	Description and Sta	<u>itus</u>					
1.	 Type of Emissions Unit Addressed in this Section: (Check one) This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent). 							
	process o	ssions Unit Informat r production units an vent) but may also p	ıd ac	ctivities wh	ich l	has at least one de		
		ssions Unit Informat cess or production un						
2.	 Description of Emissions Unit Addressed in this Section: Municipal Waste Combustor & Auxiliary Burners-Unit No. 1 							
3.	Emissions U	nit Identification Nu	mbe	r: 103				
4.	Emissions Unit Status Code: A	5. Commence Construction Date:	6.	Initial Startup Date: 08/30/01	7.	Emissions Unit Major Group SIC Code: 49	8.	Acid Rain Unit? ☐ Yes ☑ No
9.	Package Unit Manufacture	t: r: D.B. Riley			Мо	del Number: 275	3	
10	. Generator N	Iameplate Rating: 2	2.5	MW				
11	11. Emissions Unit Comment: Excess emissions are allowed during startup, shutdown, or malfunction, provided that the duration of these events does not exceed 3 hours per occurrence. For CO compliance, the duration of a malfunction period is limited to 15 hours per occurrence. (40 CFR 60 Subparts Cb and Eb)							

Emissions Unit Control Equipment

1.	Control Equipment/Method(s) Description:							
	This emissions unit is equipped with a spray dryer absorber (SDA), activated carbon injection system, fabric filter baghouse, and selective non-catalytic reduction (SNCR).							
2.	Control Device or Method Code(s): 016, 048, 067, 107							

B. EMISSIONS UNIT CAPACITY INFORMATION

(Optional for unregulated emissions units.)

Emissions Unit Operating Capacity and Schedule

1.	Maximum Process or Throughput Rate:	
2.	Maximum Production Rate:	
3.	Maximum Heat Input Rate: 120 MMBtu/hr (see item 6)	
4.	Maximum Incineration Rate:	
	288 tons/day	
5.	Requested Maximum Operating Schedule:	
	24 hours/day	7 days/week
	52 weeks/year	8.760 hours/year

6. Operating Capacity/Schedule Comment:

120 MMBtu heat input rate for informational purposes only, not for compliance. Maximum steam flow and nominal capacity are limited by Florida permit no. PSD-FL-086(A).

C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

Emission Point Description and Type

	. Identification of Point on Plot Plan or Flow Diagram: See Exhibit 1		2. Emission Point Type Code: 1				
3. Descriptions of E	Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking:						
Not Applicable							
4. ID Numbers or D	escription	ns of Emission Un	nits with this Emission	n Point in Common:			
Not Applicable							
5. Discharge Type (V	Code:	6. Stack Height 201 feet	•	7. Exit Diameter: 4.2 feet			
8. Exit Temperature 315°F	: :	9. Actual Volum 60,894 acfm	netric Flow Rate:	10. Water Vapor: 20% ±			
11. Maximum Dry S 36,686 dscfm	tandard Fl	low Rate:	12. Nonstack Emission Point Height:				
13. Emission Point U Zone: 17 Ea	JTM Coor ast (km):	rdinates 360.0	14. Emission Point Latitude/Longitude Latitude (DD/MM/SS)				
N	orth (km):	3091.9	Longitude (DD/MM/SS)				
15. Emission Point C	Comment:						
Four MWCs have separate stacks (flues) located within a common enclosure.							
·							

D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment Description and Rate: Segment 1 of 2

	·						
1.	. Segment Description (Process/Fuel Type):						
	Solid Waste Disposal – Government Municipal Incineration – Stationary Mass Burn Waterwall Combustor						
2.	Source Classification Code	e (SC	CC):	3. SCC Units:			
	50100105			Tons Burned (all solid fuels)			
4.	Maximum Hourly Rate:	5.	Maximum Annual Rate:		6. Estimated Annual Activi		
	See item 10		See item 10)		Factor:	
7.	Maximum % Sulfur:	8.	Maximum '	% Ash:	9.	Million Btu per SCC Unit:	
	N/A		N/A			10±	
10. Segment Comment:							
	PSD-FL-086(A) limits nominal heat input to 104 MMBtu/hr and nominal capacity to 250						
	tons per day (rolling 12-m	onth	average).				

Segment Description and Rate: Segment 2 of 2

<u>50,</u>	Segment Description and Nate: Segment 2 of 2						
1.	. Segment Description (Process/Fuel Type):						
	Solid Waste Disposal – Government Auxiliary Fuel/No Emissions – Natural Gas						
2.	. Source Classification Code (SCC): 50190006			3. SCC Units: Million Cubic Feet Burned (all gaseous fuels)			
4.	Maximum Hourly Rate: See item 10	5.	Maximum A	Ann	nual Rate:	6.	Estimated Annual Activity Factor:
7.	Maximum % Sulfur: N/A	8.	Maximum % Ash: N/A		ish:	9.	Million Btu per SCC Unit: 1,027±
10	10. Segment Comment: PSD-FL-086(A) limits the maximum hourly rate by the 10% annual capacity factor.						

E. EMISSIONS UNIT POLLUTANTS

List of Pollutants Emitted by Emissions Unit

1. Pollutant Emitted	2. Primary Control	3. Secondary Control	4. Pollutant
	Device Code	Device Code	Regulatory Code
PM	016		EL
SO2	067	016	EL
NOX	107		EL
CO			EL
HCL (H106)	067	016	EL
H107	016		EL
PB	016		EL
H021	016		EL
H114	048		EL
DIOX	067	016	EL
H027	016		EL

POLLUTANT DETAIL INFORMATION
Page [1] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: PM	2. Total Percent Eff	Ficiency of Control:
3.	Potential Emissions:	4. Sy	ynthetically Limited?
	2.76 lb/hour 12.1	tons/year] Yes √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):	
6.	Emission Factor: 27 mg/dscm, corrected to	7% O ₂	7. Emissions Method Code:
	Reference: PSD-FL-086(A)		0
8.	Calculation of Emissions:		
9.	Limited by Florida permit PSD-FL-086(A) Pollutant Potential/Estimated Fugitive Emis	sions Comment:	
) y.	romain rotential/Estimated rugitive Emis	sions Comment:	
	Limited by Florida permit PSD-FL-086(A)		

POLLUTANT DETAIL INFORMATION Page [2] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: SO2	2. Total Percent Efficiency of Control:			
3.	Potential Emissions:		4. Syntl	netically Limited?	
	lb/hour	tons/year		'es √ No	
5.	Range of Estimated Fugitive Emissions (as	applicable):			
6.	Emission Factor: 29 ppmdv or 75% remova	al, corrected to	7% O ₂	7. Emissions Method Code:	
	Reference: PSD-FL-086(A)			0	
8.	Calculation of Emissions:	•			
	Limited by Florida permit PSD-FL-086(A)				
				•	
9.	Pollutant Potential/Estimated Fugitive Emis	ssions Commen	it:		
	Florida permit PSD-FL-086(A) limits SO_2 emissions to 29 ppmdv or 25% of the potential sulfur dioxide emission (75% reduction by weight or volume), corrected to 7% O_2 , whichever is less stringent. Facility-wide SO_2 emissions limited to 460 tons/year.				

POLLUTANT DETAIL INFORMATION Page [3] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: NOX	2. Total Percent Efficiency of Control:			
3.	Potential Emissions:		4. Synth	etically Limited?	
	40.1 lb/hour	tons/year	Y	es √ No	
5.	Range of Estimated Fugitive Emissions (as	applicable):			
6.	Emission Factor: 205 ppmdv, corrected to	7% O ₂		7. Emissions Method Code:	
	Reference: PSD-FL-086(A)			0	
8.	Calculation of Emissions:				
	Limited by Florida permit PSD-FL-086(A)	aiona Gamma			
9.	Limited by Florida permit PSD-FL-086(A), which also contains additional emission limit of 0.335 lb/MMBtu. Facility-wide NO _X emissions limited to 679 tons/year.				

POLLUTANT DETAIL INFORMATION
Page [4] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: CO	2. Total Percent Efficiency of Control:				
3.	Potential Emissions:		4. Synth	etic	ally Limited?	
	11.91 lb/hour	tons/year	Y	es	√ No	
5.	Range of Estimated Fugitive Emissions (as	applicable):				
6.	Emission Factor: 100 ppmdv, corrected to	7% O ₂		7.	Emissions Method Code:	
	Reference: PSD-FL-086(A)				0	
8.	Calculation of Emissions:			•		
	Limited by Florida permit PSD-FL-086(A)					
	Elimited by Florida perimit 13D-1 E-000(A)					
9.	Pollutant Potential/Estimated Fugitive Emis	sions Commen	t:			
	Limited by Florida permit PSD-FL-086(A), which also contains additional emission limit of 0.0995 lb/MMBtu. Facility-wide CO emissions limited to 185 tons/year.					

POLLUTANT DETAIL INFORMATION Page [5] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: HCL (H106)	2. Total Perc	ent Efficie	ency of Control:
3.	Potential Emissions:		4. Synth	etically Limited?
	lb/hour 67.9	tons/year	Y	es No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 29 ppmdv or 95% remova	al, corrected to	7% O ₂	7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:			
0	Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment	:	
	Florida permit PSD-FL-086(A) limits HCL emissions to 29 ppmdv or 5 % of the potential sulfur dioxide emission (95% reduction by weight or volume), corrected to 7% O_2 , whichever is less stringent.			

POLLUTANT DETAIL INFORMATION Page [6] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: H107 (Fluoride (as HF))	2. Total Percent Efficie	ency of Control:
3.	Potential Emissions:	4. Synth	netically Limited?
	1.5 lb/hour 6.57	tons/year Y	es √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):	
6.	Emission Factor:	_	7. Emissions Method Code:
	Reference: PSD-FL-086(A)		0
8.	Calculation of Emissions:		
0	Limited by Florida permit PSD-FL-086(A)	sions Comment:	
9.	Pollutant Potential/Estimated Fugitive Emis Limited by Florida permit PSD-FL-086(A), of 0.0125 lb/MMBtu.		tional emission limit

POLLUTANT DETAIL INFORMATION
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F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: PB	2. Total Perc	ent Efficie	ency	of Control:
3.	Potential Emissions:		4. Synth	etic	ally Limited?
	0.0451 lb/hour 0.197	7 tons/year	☐ Y	es	√ No
5.	Range of Estimated Fugitive Emissions (as	applicable):			
6.	Emission Factor: 0.44 mg/dscm, corrected to	to 7% O ₂		7.	Emissions Method Code:
	Reference: PSD-FL-086(A)				0
8.	Calculation of Emissions:				
9.	Limited by Florida permit PSD-FL-086(A) Pollutant Potential/Estimated Fugitive Emis	sions Commen	t:		
, <i>2</i> .	Pollutant Potential/Estimated Fugitive Emissions Comment: Limited by Florida permit PSD-FL-086(A), which also contains additional emission limit of 3.76E-04 lb/MMBtu.				

POLLUTANT DETAIL INFORMATION Page [8] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: H021 (Beryllium Compounds)	2. Total Percent	Efficie	ncy of Control:
3.	Potential Emissions: 0.000115 lb/hour 5.04E-04	4. 4 tons/year	Synth Y	etically Limited? es √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor:	-		7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:			
	Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis Limited by Florida permit PSD-FL-086(A), of 9.58E-07 lb/MMBtu.		ns addit	ional emission limit

POLLUTANT DETAIL INFORMATION
Page [9] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted:			ency of Control:
	H114 (Mercury Compounds)		,	
3.	Potential Emissions:		4. Synth	etically Limited?
	lb/hour 0.0605	5 tons/year	□ Y	es √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: $0.070 \text{ mg/dscm or } 85\% \text{ re} 7\% \text{ O}_2$	0.070 mg/dscm or 85% reduction, corrected to		7. Emissions Method Code: 0
	Reference: PSD-FL-086(A)			
8.	. Calculation of Emissions:			
0	Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment	t:	
	Florida permit PSD-FL-086(A) limits H114 emissions to 0.070 mg/dscm or 15 % of the potential mercury emission concentration (85% reduction by weight or volume), corrected to 7% O ₂ , whichever is less stringent.			

POLLUTANT DETAIL INFORMATION Page [10] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: DIOX	2. Total Percent	Efficie	ncy of Control:
3.	Potential Emissions:		Synth	etically Limited?
	3.07E-06 lb/hour 1.35E-05	5 tons/year	☐ Y	es √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 30 ng/dscm (total mass), o	corrected to 7% O ₂		7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:			
Q	Limited by Florida permit PSD-FL-086(A) Pollutant Potential/Estimated Engitive Emis	sions Comment		
· 9.	Pollutant Potential/Estimated Fugitive Emis Limited by Florida permit PSD-FL-086(A), of 2.56E-08 lb/MMBtu.		ns addit	ional emission limit

POLLUTANT DETAIL INFORMATION
Page [11] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted:	2. Total Percent Efficient	ency of Control:
<u></u>	H027 (Cadmium Compounds)		
3.	Potential Emissions:	4. Syntl	hetically Limited?
	4.10E-03 lb/hour 0.0179	tons/year Y	Yes √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):	
6.	Emission Factor: 0.040 mg/dscm, corrected	l to 7% O ₂	7. Emissions Method Code:
	Reference: PSD-FL-086(A)		0
8.	Calculation of Emissions:		
	Limited by Florida permit PSD-FL-086(A)		
9.	Pollutant Potential/Estimated Fugitive Emis Limited by Florida permit PSD-FL-086(A), of 3.42E-05 lb/MMBtu.	•	tional emission limit

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 1 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Emissions:	Allowable
3.	Allowable Emissions and Units: 27 mg/dscm, corrected to 7% O ₂	4.	Equivalent Allowable En 2.76 lb/hour	nissions: 12.1 tons/year
5.	 Method of Compliance: Compliance with PM emission limits will be demonstrated annually using EPA Reference Method 5. 			. Reference Method
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A)	Oper	ating Method):	

Allowable Emissions 2 of 11

Basis for Allowable Emissions Code: RULE	2. Future Effective Date of Allowable Emissions:	
3. Allowable Emissions and Units: 29 ppmdv or 75% removal, corrected to 7% O ₂	4. Equivalent Allowable Emissions: lb/hour tons/year	
Method of Compliance: Compliance with SO ₂ emission limits will be demonstrated via CEMS using EPA Reference Method 19 to calculate the daily geometric average SO ₂ concentration.		
Allowable Emissions Comment (Description of Operating Method): Florida permit PSD-FL-086(A) limits SO ₂ emissions to 29 ppmdv or 25 % of the potential sulfur dioxide emission (75% reduction by weight or volume), corrected to 7% O ₂ , whichever is less stringent. Facility-wide SO ₂ emissions limited to 460 tons/year.		

Allowable Emissions 3 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units: 205 ppmdv, corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 40.1 lb/hour tons/year	
5.	5. Method of Compliance: Compliance with NO _x emission limits will be demonstrated via CEMS using EPA Reference Method 19 to calculate the daily arithmetic average NO _x concentration.			
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A). Faci		•	

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 4 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 100 ppmdv, corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 11.9 lb/hour tons/year
5.	5. Method of Compliance: Compliance with CO emission limits will be demonstrated via CEMS using a 4-hour block average.		
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A). Fac		

Allowable Emissions 5 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Emissions:	Allowable
3.	Allowable Emissions and Units: 29 ppmdv or 95% removal, corrected to 7% O ₂	4.	Equivalent Allowable En lb/hour	nissions: 67.9 tons/year
5.	Method of Compliance: Compliance with HCL emission limits will be demonstrated annually using EPA Reference Method 26 or 26A.			
6.	6. Allowable Emissions Comment (Description of Operating Method): Florida permit PSD-FL-086(A) limits HCL emissions to 29 ppmdv or 5 % of the potential sulfur dioxide emission (95% reduction by weight or volume), corrected to 7% O ₂ , whichever is less stringent.			

Allowable Emissions Allowable Emissions 6 of 11

1.	Basis for Allowable Emissions Code: RULE	2. Future Effective Date of Allowable Emissions:				
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions:				
	1.5 lb/hour	6.57 tons/year				
5.	Method of Compliance: Compliance with H107 (Fluoride (as HF)) emission limits will be demonstrated every 5 years using EPA Reference Method 13A or 13B.					
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A), which 0.0125 lb/MMBtu.					

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 7 of 11

1.	Basis for Allowable Emissions Code: RULE	Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units: 0.44 mg/dscm, corrected to 7% O ₂	4. Equivalent Allowable Emissions: 0.0451 lb/hour 0.197 tons/year	
5.	. Method of Compliance: Compliance with PB emission limits will be demonstrated annually using EPA Reference Method 29.		
6.	Allowable Emissions Comment (Description of Operating Method): Limited by Florida permit PSD-FL-086(A), which also contains additional emission limit of 3.76E-04 lb/MMBtu.		

Allowable Emissions 8 of 11

		
1.	Basis for Allowable Emissions Code: RULE	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 0.000115 lb/hour	4. Equivalent Allowable Emissions: 5.04E-04 tons/year
5.	. Method of Compliance: Compliance with H021 (Beryllium Compounds) emission limits will be demonstrated every 5 years using EPA Reference Method 29.	
6.	. Allowable Emissions Comment (Description of Operating Method): Limited by Florida permit PSD-FL-086(A), which also contains additional emission limit of 9.58E-07 lb/MMBtu.	

Allowable Emissions 2 of 11

1. Basis for Allowable Emissions Code:

	RULE	Emissions:	
3	6. Allowable Emissions and Units: 0.070 mg/dscm or 85% removal, @ 7% O ₂	Equivalent Allowable Emissions: Ib/hour 0.0605 tons/year	
-	Method of Compliance: Compliance with H114 (Mercury Compounds) emission limits will be demonstrated annually using EPA Reference Method 29.		
	Allowable Emissions Comment (Description of Operating Method): Florida permit PSD-FL-086(A) limits H114 emissions to 0.070 mg/dscm or 15 % of the potential mercury emission concentration (85% reduction by weight or volume), corrected to 7% O ₂ , whichever is less stringent.		

2. Future Effective Date of Allowable

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 10 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 30 ng/dscm (total mass), corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 3.07E-06 lb/hour 1.35E-05 tons/year
5.	. Method of Compliance: Compliance with DIOX emission limits will be demonstrated annually using EPA Reference Method 23.		
6.	Allowable Emissions Comment (Description of Operating Method): Limited by Florida permit PSD-FL-086(A), which also contains additional emission limit of 2.56E-08 lb/MMBtu.		

Allowable Emissions Allowable Emissions 11 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 0.040 mg/dscm, corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 4.10E-03 lb/hour, 3.42E-05 lb/MMBtu 0.0179 tons/year
5.	Method of Compliance: Compliance with H027 (Cadmium Compounds) emission limits will be demonstrated annually using EPA Reference Method 29.		
6.	Allowable Emissions Comment (Description of Operating Method): Limited by Florida permit PSD-FL-086(A)		

G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

<u>Visible Emissions Limitation:</u> Visible Emissions Limitation <u>1</u> of <u>1</u>

Visible Emissions Subtype: VE10	2. Basis for Allowable Opacity:√ Rule ☐ Other	
Normal Conditions: 10 % Ex	ceptional Conditions: 100 % ed: 3 hours	
	determining compliance with the opacity limit	
. Visible Emissions Comment: Excess emissions are allowed during startup, shut-down or malfunction, provided that the duration of these events does not exceed 3 hours (40 CFR 60.56(b)).		
<u>Visible Emissions Limitation:</u> Visible Emissions Limitation of		
Visible Emissions Subtype:	2. Basis for Allowable Opacity: Rule Other	
Normal Conditions: % Ex	ceptional Conditions: % ed: min/hour	
Method of Compliance:		
Visible Emissions Comment:		
	Allowable Opacity: Normal Conditions: 10 % Ex Maximum Period of Excess Opacity Allower Method of Compliance: EPA Reference Method 9 shall be used for except as provided under 40 CFR 60.11(e). Visible Emissions Comment: Excess emissions are allowed during starture duration of these events does not exceed 3 has been been been been been been been bee	

H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

Continuous Monitoring System: Continuous Monitor 1 of 3

1.	Parameter Code:	2. Pollutant(s):		
	VE	Visible Emissions (Opacity)		
3.	CMS Requirement:			
4.				
	Manufacturer: Land			
	Model Number: 4500 MK II +	Serial Number: 0095466		
5.	Installation Date:	6. Performance Specification Test Date:		
7.	Continuous Monitor Comment:			
ļ	Manianalana da Pabaia Pilan anda			
	Monitor located at Fabric Filter outlet			
<u>Co</u>	Continuous Monitoring System: Continuous Monitor 2 of 3			
1.	Parameter Code:	2. Pollutant(s):		
	EM, TEMP, FLOW	SO ₂ , O ₂ , Temperature, Steam Flow		
3.	CMS Requirement:	√ Rule		
4.	Monitor Information	_		
	Manufacturer: Sick			
	Model Number: MCS100EHW	Serial Number: 193		
5.	Installation Date:	6. Performance Specification Test Date:		
7.	Continuous Monitor Comment:			
	Monitor located at SDA inlet			
	Tromor routed at ODI i linet			
1				
		·		

H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

Continuous Monitoring System: Continuous Monitor 3 of 3

I.	Parameter Code:	2. Pollutant(s):			
	EM, TEMP, FLOW	O_2 , NO_x , CO , SO_2 , Temperature,			
		Steam Flow			
3.	CMS Requirement:	√ Rule			
4.	Monitor Information				
	Manufacturer: Sick				
	Model Number: MCS100EHW	Serial Number: 197			
5.	Installation Date:	6. Performance Specification Test Date:			
7.	Continuous Monitor Comment:				
	Monitor located at Fabric Filter outlet				
		·			
Continuous Monitoring System: Continuous Monitor _ of _					
<u>Co</u>	ontinuous Monitoring System: Continuous M	Ionitor _ of _			
	Parameter Code: Continuous Monitoring System: Continuous M	Ionitor _ of _ 2. Pollutant(s):			
1.	Parameter Code:	2. Pollutant(s):			
1.	Parameter Code: CMS Requirement:				
1.	Parameter Code: CMS Requirement: [Monitor Information	2. Pollutant(s):			
3.	Parameter Code: CMS Requirement: [Monitor Information Manufacturer:	2. Pollutant(s): Rule			
3.	Parameter Code: CMS Requirement: [Monitor Information Manufacturer: Model Number:	2. Pollutant(s):			
3.	Parameter Code: CMS Requirement: [Monitor Information Manufacturer: Model Number:	2. Pollutant(s): Rule			
3. 4.	Parameter Code: CMS Requirement: [Monitor Information Manufacturer: Model Number: Installation Date:	2. Pollutant(s): Rule Other Serial Number:			
3. 4.	Parameter Code: CMS Requirement: [Monitor Information Manufacturer: Model Number: Installation Date:	2. Pollutant(s): Rule Other Serial Number:			
3. 4.	Parameter Code: CMS Requirement: [Monitor Information Manufacturer: Model Number: Installation Date:	2. Pollutant(s): Rule Other Serial Number:			
3. 4.	Parameter Code: CMS Requirement: [Monitor Information Manufacturer: Model Number: Installation Date:	2. Pollutant(s): Rule Other Serial Number:			
3. 4.	Parameter Code: CMS Requirement: [Monitor Information Manufacturer: Model Number: Installation Date:	2. Pollutant(s): Rule Other Serial Number:			
3. 4.	Parameter Code: CMS Requirement: [Monitor Information Manufacturer: Model Number: Installation Date:	2. Pollutant(s): Rule Other Serial Number:			

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 2 Previously Submitted, Date
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 8 Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 9 Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)
	✓ Attached, Document ID: Exhibit 10
5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Value Previously Submitted, Date Previously Submit
6.	Compliance Demonstration Reports/Records Attached, Document ID:
	Test Date(s)/Pollutant(s) Tested:
	Previously Submitted, Date: November 18, 2005
	Test Date(s)/Pollutant(s) Tested: 2005 compliance testing results and 2004 Statement of Compliance are included in Exhibit 12. To be Submitted, Date (if known):
	Test Date(s)/Pollutant(s) Tested: Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute Attached, Document ID:

Additional Requirements for Air Construction Permit Applications

1.	Control Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7),
	F.A.C.; 40 CFR 63.43(d) and (e)) Attached, Document ID: Not Applicable
2.	
2.	Rule 62-212.500(4)(f), F.A.C.)
	Attached, Document ID: Not Applicable
3.	Description of Stack Sampling Facilities (Required for proposed new stack sampling
	facilities only)
	Attached, Document ID: Not Applicable
Ad	Iditional Requirements for Title V Air Operation Permit Applications
1.	Identification of Applicable Requirements
	√ Attached, Document ID: Exhibit 5
2.	Compliance Assurance Monitoring
_	✓ Attached, Document ID: Exhibit 6 Not Applicable
3.	Alternative Methods of Operation
	Attached, Document ID: Not Applicable
4.	Alternative Modes of Operation (Emissions Trading) Attached, Document ID: Not Applicable
5	
ال	Acid Rain Part Application Certificate of Representation (EPA Form No. 7610-1)
	Copy Attached, Document ID:
	Acid Rain Part (Form No. 62-210.900(1)(a))
	Attached, Document ID:
	Previously Submitted, Date:
	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
	Attached, Document ID:
	Previously Submitted, Date:
	New Unit Exemption (Form No. 62-210.900(1)(a)2.)
	Attached, Document ID:
	Previously Submitted, Date:
	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.) Attached, Document ID:
	Previously Submitted, Date:
	Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)
	Attached, Document ID:
	Previously Submitted, Date:
	Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)
	Attached, Document ID:
	Previously Submitted, Date:
	√ Not Applicable

Additional Requirements Commen	<u>ու</u>	
None		

A. GENERAL EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Emissions Unit Classification

1.	Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)								
	 ✓ The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit. ☐ The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit. 								
En	nissions Unit	Description and Sta	tus						
1.	Type of Emis	ssions Unit Addresse	d in	this Sectio	n: (Check one)			
	process o	ssions Unit Informat r production unit, or s at least one definab	acti	vity, which	pro	duces one or more		_	
	process o	ssions Unit Informat r production units an vent) but may also p	d ac	ctivities wh	ich l	has at least one de			
		ssions Unit Informat cess or production ur				•			
2.	Description of	of Emissions Unit Ad	dre	ssed in this	Sec	tion:			
	Municipal W	aste Combustor & A	uxi	liary Burne	rs-U	Init No. 2			
3.	Emissions U	nit Identification Nur	nbe	r: 104					
4.	Emissions Unit Status Code: A	5. Commence Construction Date:	6.	Initial Startup Date: 08/30/01	7.	Emissions Unit Major Group SIC Code: 49	8.	Acid Rain Unit? ☐ Yes ☑ No	
9.	Package Unit				١.,	1127 1 275	_		
10	Manufacturer Generator N		2 5	MW	Mo	del Number: 275	4		
	10. Generator Nameplate Rating: 22.5 MW 11. Emissions Unit Comment:								
	duration of th	sions are allowed dur nese events does not malfunction period i	exc	eed 3 hours	per	occurrence. For	CÔ	compliance, the	

Emissions Unit Control Equipment

1.	Control Equipment/Method(s) Description:							
	This emissions unit is equipped with a spray dryer absorber (SDA), activated carbon injection system, fabric filter baghouse, and selective non-catalytic reduction (SNCR).							
2.	Control Device or Method Code(s): 016, 048, 067, 107							

B. EMISSIONS UNIT CAPACITY INFORMATION

(Optional for unregulated emissions units.)

Emissions Unit Operating Capacity and Schedule

1.	Maximum Process or Throughput Rate:	
2.	Maximum Production Rate:	
3.	Maximum Heat Input Rate: 120 MMBtu/hr (see item 6)	
4.	Maximum Incineration Rate:	
	288 tons/day	
5.	Requested Maximum Operating Schedule:	
	24 hours/day 7 days/week	
	52 weeks/year 8,760 hours/y	ear
6.	Operating Capacity/Schedule Comment:	
	120 MMBtu heat input rate for informational purposes only, not for compliance. Maximum steam flow and nominal capacity are limited by Florida permit no. PSD-F 086(A).	L-

C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

Emission Point Description and Type

1.	Identification of Point on Plot Plan or Flow Diagram: See Exhibit 1			2. Emission Point 7	Гуре Code: 1	
3.	Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking:					
	Not Applicable					
					- · · · ·	
4.	ID Numbers or	Description	ns of Emission Ui	nits with this Emission	n Point in Common:	
	Not Applicable					
5.	Discharge Type	Code:	6. Stack Height	•	7. Exit Diameter:	
	V		201 feet		4.2 feet	
8.	Exit Temperatu	re:		metric Flow Rate:	10. Water Vapor:	
	315°F		60,894 acfm		20% ±	
11	. Maximum Dry 36,686 dscfm	Standard F	flow Rate:	12. Nonstack Emission Point Height:		
13	. Emission Point			14. Emission Point Latitude/Longitude		
		East (km):	360.0	Latitude (DD/MM/SS)		
		North (km)		Longitude (DD/I	MM/SS) 	
15	. Emission Point	Comment:				
	Four MWCs ha	ve separate	e stacks (flues) loc	cated within a common	n enclosure.	

D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment Description and Rate: Segment 1 of 2

				,			
1.	. Segment Description (Process/Fuel Type):						
	Solid Waste Disposal – Government Municipal Incineration – Stationary Mass Burn Waterwall Combustor						
2.	Source Classification Code (SCC): 50100105		3. SCC Units: Tons Burned (all solid fuels)				
4.	Maximum Hourly Rate: See item 10	5. Maximum A		6. Estimated Annual Activity Factor:			
7.	Maximum % Sulfur: N/A	8. Maximum % Ash: N/A		9. Million Btu per SCC Unit: 10±			
10	10. Segment Comment:						
	PSD-FL-086(A) limits nominal heat input to 104 MMBtu/hr and nominal capacity to 250 tons per day (rolling 12-month average).						

Segment Description and Rate: Segment 2 of 2

1.	. Segment Description (Process/Fuel Type):							
	Solid Waste Disposal – Government Auxiliary Fuel/No Emissions – Natural Gas							
2.	Source Classification Code	e (S	CC):	3. SCC Units:				
	50190006			Million Cubic Feet Burned (all gaseous				
				fuels)		-		
4.	Maximum Hourly Rate:	5.	Maximum .	Annual Rate:	6.	Estimated Annual Activity		
	See item 10					Factor:		
7.	Maximum % Sulfur:	8.	Maximum ⁶	% Ash:	9.	Million Btu per SCC Unit:		
	N/A		N/A			1,027±		
10	Segment Comment:							
	10. Segment Comment: PSD-FL-086(A) limits the maximum hourly rate by the 10% annual capacity factor.							

E. EMISSIONS UNIT POLLUTANTS

List of Pollutants Emitted by Emissions Unit

1. Pollutant Emitted	2. Primary Control	3. Secondary Control	4. Pollutant
	Device Code	Device Code	Regulatory Code
PM	016		EL
SO2	067	016	EL
NOX	107		EL
СО			EL
HCL (H106)	067	016	EL
H107	016		EL
PB	016		EL
H021	016		EL
H114	048		EL
DIOX	067	016	EL
H027	016		EL

POLLUTANT DETAIL INFORMATION
Page [1] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

Pollutant Emitted: PM	2. Total Perce	ent Efficiency of Control:
3. Potential Emissions:		4. Synthetically Limited?
2.76 lb/hour	12.1 tons/year	☐ Yes
5. Range of Estimated Fugitive Emission	ons (as applicable):	dia.
6. Emission Factor: 27 mg/dscm, corre	ected to 7% O ₂	7. Emissions Method Code:
Reference: PSD-FL-086(A)		0
8. Calculation of Emissions:	-	·
Linked by Planika and 't DCD FL (20674	
Limited by Florida permit PSD-FL-0	J86(A)	
9. Pollutant Potential/Estimated Fugitive	ve Emissions Comment	·
2. 2 oracian i otornian estimated i agitiv	o Billissions Comment	•
Limited by Florida permit PSD-FL-0)86(A)	

POLLUTANT DETAIL INFORMATION Page [2] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted:	2. Total Percent Efficiency of Control:			
	SO2				
3.	Potential Emissions:		4. Syntl	netically Limited?	
	lb/hour	tons/year	Y	es √ No	
5.	Range of Estimated Fugitive Emissions (as	applicable):			
6.	Emission Factor: 29 ppmdv or 75% remova	al, corrected to	7% O₂	7. Emissions Method Code:	
	Reference: PSD-FL-086(A)			0	
8.	Calculation of Emissions:				
0	Limited by Florida permit PSD-FL-086(A)				
9.	9. Pollutant Potential/Estimated Fugitive Emissions Comment: Florida permit PSD-FL-086(A) limits SO ₂ emissions to 29 ppmdv or 25 % of the potential sulfur dioxide emission (75% reduction by weight or volume), corrected to 7% O ₂ , whichever is less stringent. Facility-wide SO ₂ emissions limited to 460 tons/year.				

POLLUTANT DETAIL INFORMATION Page [3] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: NOX	2. Total Percent Efficiency of Control:			
3.	Potential Emissions:		4. Synth	etically Limited?	
	40.1 lb/hour	tons/year	☐ Y	es √ No	
5.	Range of Estimated Fugitive Emissions (as	applicable):			
6.	Emission Factor: 205 ppmdv, corrected to 7	1% O₂		7. Emissions Method Code:	
	Reference: PSD-FL-086(A)			0	
8.	Calculation of Emissions:				
	Limited by Florida permit PSD-FL-086(A)				
9.	Pollutant Potential/Estimated Fugitive Emis	sions Commen	t:		
	Limited by Florida permit PSD-FL-086(A), of 0.335 lb/MMBtu. Facility-wide NO _X em				

POLLUTANT DETAIL INFORMATION
Page [4] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: CO	2. Total Percent Efficiency of Control:			of Control:
3.	Potential Emissions:		4. Syntl	netic	ally Limited?
	11.91 lb/hour	tons/year	Y	es	√ No
5.	Range of Estimated Fugitive Emissions (as	applicable):			
6.	Emission Factor: 100 ppmdv, corrected to 7	7% O ₂		7.	Emissions Method Code:
	Reference: PSD-FL-086(A)				0
8.	Calculation of Emissions:				
	Limited by Florida permit PSD-FL-086(A)				
9.	Pollutant Potential/Estimated Fugitive Emis Limited by Florida permit PSD-FL-086(A),			tions	al emission limit
	of 0.0995 lb/MMBtu. Facility-wide CO emi				

POLLUTANT DETAIL INFORMATION Page [5] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: HCL (H106)	2. Total Perc	ent Efficie	ency of Control:
3.	Potential Emissions:		4. Synth	etically Limited?
	lb/hour 67.9	tons/year	□ Y	es √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 29 ppmdv or 95% remova	l, corrected to	7% O ₂	7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:			
	Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment	t:	
	Florida permit PSD-FL-086(A) limits HCL sulfur dioxide emission (95% reduction by whichever is less stringent.			

POLLUTANT DETAIL INFORMATION
Page [6] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: H107 (Fluoride (as HF))	2. Total Percent Efficiency of Control:	
3.	Potential Emissions:	4. Sy	nthetically Limited?
	1.5 lb/hour 6.57	tons/year] Yes √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):	
6.	Emission Factor:		7. Emissions Method Code:
	Reference: PSD-FL-086(A)		0
8.	Calculation of Emissions:		
	Limited by Florida permit PSD-FL-086(A)		
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment:	
	Limited by Florida permit PSD-FL-086(A), of 0.0125 lb/MMBtu.	which also contains ac	dditional emission limit

POLLUTANT DETAIL INFORMATION
Page [7] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: PB	2. Total Percent Efficiency of Control:		
3.	Potential Emissions: 0.0451 lb/hour 0.197		netically Limited? Yes	
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 0.44 mg/dscm, corrected to	co 7% O ₂	7. Emissions Method Code:	
	Reference: PSD-FL-086(A)		0	
8.	Calculation of Emissions:			
	Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment:		
	Limited by Florida permit PSD-FL-086(A), of 3.76E-04 lb/MMBtu.	which also contains addi	tional emission limit	

POLLUTANT DETAIL INFORMATION
Page [8] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted:	2. Total Percent Efficiency of Control:		
_	H021 (Beryllium Compounds)	14.0	11 T 10	
3.	Potential Emissions:	•	hetically Limited?	
	0.000115 lb/hour 5.04E-04	tons/year	Yes ✓ No	
5.	Range of Estimated Fugitive Emissions (as	applicable):		
	<u></u>		_	
6.	Emission Factor:		7. Emissions	
			Method Code:	
	Reference: PSD-FL-086(A)		0	
8.	Calculation of Emissions:	<u> </u>		
	Limited by Florida permit PSD-FL-086(A)			
	Dellutent Detectiol/Estimated Expirition Engine	-i Co		
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment:		
	Limited by Florida permit PSD-FL-086(A),	which also contains add	tional emission limit	
	of 9.58E-07 lb/MMBtu.	which also contains add	tional chiission mint	
	of 7.50L of lowering.			

POLLUTANT DETAIL INFORMATION
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F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: H114 (Mercury Compounds)	2. Total Percent Efficiency of Control:		
	Potential Emissions: 1b/hour 0.0605	5 tons/year		netically Limited? Tes √ No
5.	Range of Estimated Fugitive Emissions (as	аррисавіе):		
6.	Emission Factor: 0.070 mg/dscm or 85% re 7% O ₂	duction, correc	ted to	7. Emissions Method Code: 0
	Reference: PSD-FL-086(A)			
8.	Calculation of Emissions:			
0	Limited by Florida permit PSD-FL-086(A)	giona Common		
9.	Pollutant Potential/Estimated Fugitive Emis Florida permit PSD-FL-086(A) limits H114 potential mercury emission concentration (8 to 7% O ₂ , whichever is less stringent.	emissions to 0	.070 mg/ds	

POLLUTANT DETAIL INFORMATION
Page [10] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: DIOX	2. Total Percent Effic	iency of Control:
3.	Potential Emissions:	4. Syn	thetically Limited?
	3.07E-06 lb/hour 1.35E-05	tons/year	Yes √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):	
6.	Emission Factor: 30 ng/dscm (total mass), o	corrected to 7% O ₂	7. Emissions Method Code:
	Reference: PSD-FL-086(A)		0
8.	Calculation of Emissions:		•
	Limited by Florida permit PSD-FL-086(A)		
9.	Pollutant Potential/Estimated Fugitive Emis Limited by Florida permit PSD-FL-086(A), of 2.56E-08 lb/MMBtu.		litional emission limit

POLLUTANT DETAIL INFORMATION
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F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted:	2. Total Percent Efficiency of Control:		
	H027 (Cadmium Compounds)			·
3.	Potential Emissions:		•	netically Limited?
	4.10E-03 lb/hour 0.0179	tons/year	□ Y	es √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 0.040 mg/dscm, corrected	to $7\% O_2$		7. Emissions
	Deference: BSD EI 096(A)			Method Code:
_	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:			
	The state of the s			
	Limited by Florida permit PSD-FL-086(A)			
1				
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment	:	
	Limited by Florida permit PSD-FL-086(A),	which also con	tains addit	tional emission limit
	of 3.42E-05 lb/MMBtu.			

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 1 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units: 27 mg/dscm, corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 2.76 lb/hour 12.1 tons/year	
5.	5. Method of Compliance: Compliance with PM emission limits will be demonstrated annually using EPA Reference Method 5.			
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A)	Эрег	rating Method):	

Allowable Emissions 2 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Emissions:	Allowable	
3.	Allowable Emissions and Units: 29 ppmdv or 75% removal, corrected to 7% O ₂	4.	Equivalent Allowable En lb/hour	nissions: tons/year	
5.	5. Method of Compliance: Compliance with SO ₂ emission limits will be demonstrated via CEMS using EPA Reference Method 19 to calculate the daily geometric average SO ₂ concentration.				
6.					

Allowable Emissions 3 of 11

1	. Basis for Allowable Emissions Code: RULE	Future Effective Date of Allowable Emissions:
3	. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:
	205 ppmdv, corrected to 7% O ₂	40.1 lb/hour tons/year
5	 Method of Compliance: Compliance with NO_X emission limits will be de Method 19 to calculate the daily arithmetic avera 	· ·
6	` 1	Operating Method): lity-wide NO _X emissions limited to 679 tons/year.

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 4 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 100 ppmdv, corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 11.9 lb/hour tons/year
5.	Method of Compliance: Compliance with CO emission limits will be den average.	nons	trated via CEMS using a 4-hour block
6.	Allowable Emissions Comment (Description of CLimited by Florida permit PSD-FL-086(A). Fac		

Allowable Emissions 5 of 11

1.	RULE	2.	Emissions:	e of Allowable
3.	Allowable Emissions and Units: 29 ppmdv or 95% removal, corrected to 7% O ₂	4.	Equivalent Allowable lb/hour	e Emissions: 67.9 tons/year
5.	Method of Compliance: Compliance with HCL emission limits will be de Method 26 or 26A.	mon	strated annually using	EPA Reference
6.	Allowable Emissions Comment (Description of C Florida permit PSD-FL-086(A) limits HCL emiss dioxide emission (95% reduction by weight or vo stringent.	sions	to 29 ppmdv or 5 %	

Allowable Emissions 6 of 11

1.	Basis for Allowable Emissions Code: RULE	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 1.5 lb/hour	4. Equivalent Allowable Emissions: 6.57 tons/year
5.	Method of Compliance: Compliance with H107 (Fluoride (as HF)) emiss EPA Reference Method 13A or 13B.	ion limits will be demonstrated every 5 years using
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A), whice 0.0125 lb/MMBtu.	

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 7 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 0.44 mg/dscm, corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 0.0451 lb/hour 0.197 tons/year
5.	Method of Compliance: Compliance with PB emission limits will be dem 29.	onst	rated annually using EPA Reference Method
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A), which 3.76E-04 lb/MMBtu.		

Allowable Emissions Allowable Emissions 8 of 11

1.	Basis for Allowable Emissions Code: RULE	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 0.000115 lb/hour	4. Equivalent Allowable Emissions: 5.04E-04 tons/year
5.	Method of Compliance: Compliance with H021 (Beryllium Compounds) years using EPA Reference Method 29.	emission limits will be demonstrated every 5
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A), whice 9.58E-07 lb/MMBtu.	

Allowable Emissions 9 of 11

1. Basis for Allowable Emissions Code:

	RULE	Emissions:
(3. Allowable Emissions and Units: 0.070 mg/dscm or 85% removal, @ 7% O ₂	4. Equivalent Allowable Emissions: lb/hour 0.0605 tons/year
	 Method of Compliance: Compliance with H114 (Mercury Compounds) et EPA Reference Method 29. 	mission limits will be demonstrated annually using
•	 Allowable Emissions Comment (Description of C Florida permit PSD-FL-086(A) limits H114 emis mercury emission concentration (85% reduction whichever is less stringent. 	sions to 0.070 mg/dscm or 15 % of the potential

2. Future Effective Date of Allowable

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 10 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 30 ng/dscm (total mass), corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 3.07E-06 lb/hour 1.35E-05 tons/year
5.	Method of Compliance: Compliance with DIOX emission limits will be did Method 23.	iemo	onstrated annually using EPA Reference
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A), whice 2.56E-08 lb/MMBtu.		

Allowable Emissions 11 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 0.040 mg/dscm, corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 4.10E-03 lb/hour, 3.42E-05 lb/MMBtu 0.0179 tons/year
5.	Method of Compliance: Compliance with H027 (Cadmium Compounds) emission limits will be demonstrated annually using EPA Reference Method 29.		
6.			
	Limited by Florida permit PSD-FL-086(A)		

G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

<u>Visible Emissions Limitation:</u> Visible Emissions Limitation <u>1</u> of <u>1</u>

1.	Visible Emissions Subtype: VE	2. Basis for Allowable Opacity: √ Rule Other	
3.	Allowable Opacity: Normal Conditions: 10 % Ex Maximum Period of Excess Opacity Allower	acceptional Conditions: 100 % a hours	
4.	Method of Compliance: EPA Reference Method 9 shall be used for except as provided under 40 CFR 60.11(e).	determining compliance with the opacity	limit
5.	Visible Emissions Comment: Excess emissions are allowed during startup duration of these events does not exceed 3 h		at the
Vis	sible Emissions Limitation: Visible Emissi	ons Limitation of	
	Total Ellings Color Ellings		
	Visible Emissions Subtype:	2. Basis for Allowable Opacity: Rule Other	
1.	Visible Emissions Subtype: Allowable Opacity:	2. Basis for Allowable Opacity: Rule Other cceptional Conditions: %	
3.	Visible Emissions Subtype: Allowable Opacity: Normal Conditions: % Ex	2. Basis for Allowable Opacity: Rule Other cceptional Conditions: %	

H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

Continuous Monitoring System: Continuous Monitor <u>1</u> of <u>3</u>

1.	Parameter Code: VE	2. Pollutant(s): Visible Emissions (Opacity)
3.	CMS Requirement:	√ Rule
4.	Monitor Information Manufacturer: Land Model Number: 4500 MK II +	Serial Number: 9995460
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
	Monitor located at Fabric Filter outlet	
		•
<u>Co</u>	ontinuous Monitoring System: Continuous	Monitor $\underline{2}$ of $\underline{3}$
1.	Parameter Code: EM, TEMP, FLOW	2. Pollutant(s): SO ₂ , O ₂ , Temperature, Steam Flow
3.	CMS Requirement:	V Rule ☐ Other
4.	Monitor Information Manufacturer: Sick	
	Model Number: MCS100EHW	Serial Number: 186
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
	Monitor located at SDA inlet	
		•

H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

<u>Continuous Monitoring System:</u> Continuous Monitor <u>3</u> of <u>3</u>

1.	Parameter Code:	2. Poll	utant(s):
	EM, TEMP, FLOW	O2,	NO_x , CO, SO ₂ , Temperature,
		Stea	m Flow
3.	CMS Requirement:	√ Rule	☐ Other
4.	Monitor Information		
	Manufacturer: Sick		
	Model Number: MCS100EHW	Seria	al Number: 196
5.	Installation Date:	6. Perf	ormance Specification Test Date:
7.	Continuous Monitor Comment:		
	Montan In coard of Palacie Pilean coales		
	Monitor located at Fabric Filter outlet		
Co	ntinuous Monitoring System: Continuous Mo	onitor of	
	ontinuous Monitoring System: Continuous Mo		
	ontinuous Monitoring System: Continuous Mo		utant(s):
1.	Parameter Code:	2. Poll	utant(s):
1. 3.	Parameter Code: CMS Requirement:		
1. 3.	Parameter Code: CMS Requirement:	2. Poll	utant(s):
1. 3.	Parameter Code: CMS Requirement: Monitor Information Manufacturer:	2. Poll	utant(s):
1. 3.	Parameter Code: CMS Requirement:	2. Poll	utant(s):
 3. 4. 	Parameter Code: CMS Requirement: Monitor Information Manufacturer:	2. Poll Rule	utant(s):
 3. 4. 5. 	Parameter Code: CMS Requirement: Monitor Information Manufacturer: Model Number: Installation Date:	2. Poll Rule	utant(s): Other al Number:
 3. 4. 5. 	Parameter Code: CMS Requirement: Monitor Information Manufacturer: Model Number:	2. Poll Rule	utant(s): Other al Number:
 3. 4. 5. 	Parameter Code: CMS Requirement: Monitor Information Manufacturer: Model Number: Installation Date:	2. Poll Rule	utant(s): Other al Number:
 3. 4. 5. 	Parameter Code: CMS Requirement: Monitor Information Manufacturer: Model Number: Installation Date:	2. Poll Rule	utant(s): Other al Number:
 3. 4. 5. 	Parameter Code: CMS Requirement: Monitor Information Manufacturer: Model Number: Installation Date:	2. Poll Rule	utant(s): Other al Number:
 3. 4. 5. 	Parameter Code: CMS Requirement: Monitor Information Manufacturer: Model Number: Installation Date:	2. Poll Rule	utant(s): Other al Number:
 3. 4. 5. 	Parameter Code: CMS Requirement: Monitor Information Manufacturer: Model Number: Installation Date:	2. Poll Rule	utant(s): Other al Number:

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 2 Previously Submitted, Date
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 8 Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 9 Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 10 Previously Submitted, Date
	Not Applicable (construction application)
5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) V Attached, Document ID: Exhibit 11 Previously Submitted, Date Not Applicable
6.	Compliance Demonstration Reports/Records Attached, Document ID:
	Test Date(s)/Pollutant(s) Tested:
	Previously Submitted, Date: November 18, 2005
	Test Date(s)/Pollutant(s) Tested: 2005 compliance testing results and 2004 Statement of Compliance are included in Exhibit 12. To be Submitted, Date (if known):
	Test Date(s)/Pollutant(s) Tested: Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	<u> </u>
	Attached, Document ID: Not Applicable

Additional Requirements for Air Construction Permit Applications

1	1. Control Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7),				
*.	F.A.C.; 40 CFR 63.43(d) and (e))				
	Attached, Document ID: \[\sqrt{Not Applicable} \]				
2.					
	Rule 62-212.500(4)(f), F.A.C.)				
	☐ Attached, Document ID: Not Applicable				
3.	Description of Stack Sampling Facilities (Required for proposed new stack sampling				
	facilities only)				
	Attached, Document ID: Not Applicable				
Ac	dditional Requirements for Title V Air Operation Permit Applications				
1.	Identification of Applicable Requirements				
	√ Attached, Document ID: Exhibit 5				
2.	Compliance Assurance Monitoring				
	Attached, Document ID: Exhibit 6 Not Applicable				
3	Alternative Methods of Operation				
"	☐ Attached, Document ID: Not Applicable				
4.	Alternative Modes of Operation (Emissions Trading)				
	Attached, Document ID: Not Applicable				
5.	Acid Rain Part Application				
	Certificate of Representation (EPA Form No. 7610-1)				
	Copy Attached, Document ID:				
	Acid Rain Part (Form No. 62-210.900(1)(a))				
	Attached, Document ID:				
	Previously Submitted, Date:				
	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)				
	Attached, Document ID:				
	Previously Submitted, Date:				
	☐ New Unit Exemption (Form No. 62-210.900(1)(a)2.)				
	Attached, Document ID:				
	Previously Submitted, Date:				
	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)				
	Attached, Document ID:				
	Previously Submitted, Date:				
	Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)				
	Attached, Document ID:				
	Previously Submitted, Date:				
	Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)				
	Attached, Document ID:				
	Previously Submitted, Date:				
	√ Not Applicable				

Additional Requirements Comment	
None	
	•

A. GENERAL EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Emissions Unit Classification

		renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)						
I				in this Emissio	ns Unit Information S	Section is a regulated		
١		emissions u		in this Emissio	na I Init Information C	laction is on		
1			d emissions unit.	in this Emissio	ns Unit Information S	section is an		
L	17							
•			Description and Sta					
I	1.		ssions Unit Addresse		,			
I					lresses, as a single em			
I		-	r production unit, or s at least one definab	•	produces one or mor	e air pollutants and		
I				-	•	issions unit, a group of		
I					_	efinable emission point		
I		-	vent) but may also p			•		
I		This Emi	ssions Unit Informat	ion Section add	dresses, as a single em	issions unit, one or		
I		more pro	cess or production un	nits and activiti	es which produce fug	itive emissions only.		
I	2.	Description of	of Emissions Unit Ad	ldressed in this	Section:			
		Municipal W	anta Cambustan & A	:1:am. D	na IInit No. 2			
		wumcipai w	aste Combustor & A	auxinary Burne	rs-Ullit No. 3			
	3.	Emissions U	nit Identification Nur	mber: 105				
	4.	Emissions	5. Commence	6. Initial	7. Emissions Unit	8. Acid Rain Unit?		
		Unit Status	Construction	Startup	Major Group	Yes		
		Code:	Date:	Date: 08/30/01	SIC Code:	No		
	0			08/30/01	49			
	9.	Package Unit	r: D.B. Riley		Model Number: 275	9		
	10.		ameplate Rating: 2	2.5 MW	Wiodel (Validet). 273			
	_		nit Comment:					
I				-	ıtdown, or malfunctio	=		
-					per occurrence. For			
		Cb and Eb)	manunction period	13 111111160 10 13	nours per occurrence.	. (40 CFR 60 Subparts		

Emissions Unit Control Equipment

1.	. Control Equipment/Method(s) Description:				
	This emissions unit is equipped with a spray dryer absorber (SDA), activated carbon injection system, fabric filter baghouse, and selective non-catalytic reduction (SNCR).				
2.	Control Device or Method Code(s): 016, 048, 067, 107				
۷٠	Control Device of Method Code(8). 010, 040, 007, 107				

B. EMISSIONS UNIT CAPACITY INFORMATION

(Optional for unregulated emissions units.)

Emissions Unit Operating Capacity and Schedule

1.	Maximum Process or Throughput Rate:			
2.	Maximum Production Rate:	-		
3.	3. Maximum Heat Input Rate: 120 MMBtu/hr (see item 6)			
4.	4. Maximum Incineration Rate:			
	288 tons/day			
5.	Requested Maximum Operating Schedule:			
	24 hours/day	7 days/week		
	52 weeks/year	8,760 hours/year		
6.	Operating Capacity/Schedule Comment:	<u> </u>		

120 MMBtu heat input rate for informational purposes only, not for compliance. Maximum steam flow and nominal capacity are limited by Florida permit no. PSD-FL-086(A).

C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

Emission Point Description and Type

Identification of Point on Plot Plan or Flow Diagram: See Exhibit 1		2. Emission Point 7	Type Code: 1	
Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking:				
Not Applicable				
		·		
			I	
ID Numbers or Description	ns of Emission Un	nits with this Emission	n Point in Common:	
Not Applicable				
Discharge Type Code: V	6. Stack Height 201 feet	:	7. Exit Diameter: 4.2 feet	
Exit Temperature: 315°F	9. Actual Volur 60,894 acfm	netric Flow Rate:	10. Water Vapor: 20% ±	
. Maximum Dry Standard Flow Rate: 36,686 dscfm		12. Nonstack Emission Point Height:		
Emission Point UTM Coordinates Zone: 17 East (km): 360.0		14. Emission Point I Latitude (DD/M)	_atitude/Longitude M/SS)	
North (km): 3091.9		Longitude (DD/MM/SS)		
Emission Point Comment:				
Four MWCs have separate stacks (flues) located within a common enclosure.				
	Flow Diagram: See Exhibition Descriptions of Emission In Not Applicable ID Numbers or Description Not Applicable Discharge Type Code: V Exit Temperature: 315°F Maximum Dry Standard From 36,686 dscfm Emission Point UTM Coor Zone: 17 East (km): North (km) Emission Point Comment:	Flow Diagram: See Exhibit 1 Descriptions of Emission Points Comprising Not Applicable ID Numbers or Descriptions of Emission Ur Not Applicable Discharge Type Code: 6. Stack Height 201 feet Exit Temperature: 9. Actual Volur 315°F 9. Actual Volur 60,894 acfm Maximum Dry Standard Flow Rate: 36,686 dscfm Emission Point UTM Coordinates Zone: 17 East (km): 360.0 North (km): 3091.9 Emission Point Comment:	Descriptions of Emission Points Comprising this Emissions Unit is Not Applicable ID Numbers or Descriptions of Emission Units with this Emission Not Applicable Discharge Type Code: V 201 feet Exit Temperature: 315°F 9. Actual Volumetric Flow Rate: 60,894 acfm Maximum Dry Standard Flow Rate: 36,686 dscfm Emission Point UTM Coordinates Zone: 17 East (km): 360.0 North (km): 3091.9 Emission Point Comment:	

D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment Description and Rate: Segment $\underline{1}$ of $\underline{2}$

1.	Segment Description (Process/Fuel Type):				
	Solid Waste Disposal – Government Municipal Incineration – Stationary Mass Burn Waterwall Combustor				
2.	Source Classification Code (SCC): 50100105		3. SCC Units: Tons Burned (all solid fuels)		
4.	Maximum Hourly Rate: See item 10	5. Maximum See item 10		6. Estimated Annual Activity Factor:	
7.	Maximum % Sulfur: N/A	8. Maximum N/A	% Ash:	9. Million Btu per SCC Unit: 10±	
10.	10. Segment Comment:				
	PSD-FL-086(A) limits nominal heat input to 104 MMBtu/hr and nominal capacity to 250 tons per day (rolling 12-month average).				

<u>56</u>	<u>Segment Description and Rate.</u> Segment <u>2</u> or <u>2</u>					
1.	1. Segment Description (Process/Fuel Type):					
	Solid Waste Disposal – Government Auxiliary Fuel/No Emissions – Natural Gas					
2.	Source Classification Code	e (SCC):	3. SCC Units:			
	50190006		Million Cubic Feet Burned (all gaseous			
			fuels)			
4.	Maximum Hourly Rate: See item 10	5. Maximum	Annual Rate:	6. Estimated Annual Activity Factor:		
7.	Maximum % Sulfur:	8. Maximum	% Ash:	9. Million Btu per SCC Unit:		
	N/A	N/A		1,027±		
10	10. Segment Comment:					
	PSD-FL-086(A) limits the maximum hourly rate by the 10% annual capacity factor.					

E. EMISSIONS UNIT POLLUTANTS

List of Pollutants Emitted by Emissions Unit

1. Pollutant Emitted	Primary Control Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
PM	016		EL
SO2	067	016	EL
NOX	107		EL
СО			EL
HCL (H106)	067	016	EL
H107	016		EL
PB	016		EL
H021	016		EL
H114	048		EL
DIOX	067	016	EL
H027	016		EL
		_	

POLLUTANT DETAIL INFORMATION
Page [1] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: PM	2. Total Percen	t Efficie	ncy of Control:
3.	Potential Emissions:	4.	. Synth	etically Limited?
	2.76 lb/hour 12.1	l tons/year	Y	es √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 27 mg/dscm, corrected to	7% O ₂		7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:			
	Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment:		
	Limited by Florida permit PSD-FL-086(A)			

POLLUTANT DETAIL INFORMATION Page [2] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: SO2	2. Total Percent Efficiency of Control:		
3.	Potential Emissions:		4. Synth	etically Limited?
	lb/hour	tons/year	☐ Y	es 🚺 No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 29 ppmdv or 75% remova	al, corrected to	7% O ₂	7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:			
	Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emissions Comment: Florida permit PSD-FL-086(A) limits SO ₂ emissions to 29 ppmdv or 25 % of the potential sulfur dioxide emission (75% reduction by weight or volume), corrected to 7% O ₂ , whichever is less stringent. Facility-wide SO ₂ emissions limited to 460 tons/year.			

POLLUTANT DETAIL INFORMATION Page [3] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: NOX	2. Total Percent Efficiency of Control:		
3.	Potential Emissions:		4. Synth	netically Limited?
	40.1 lb/hour	tons/year	□ Y	es √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 205 ppmdv, corrected to 7	7% O ₂		7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:			
	Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis	sions Commen	t:	
	Limited by Florida permit PSD-FL-086(A), which also contains additional emission limit of 0.335 lb/MMBtu. Facility-wide NO _X emissions limited to 679 tons/year.			

POLLUTANT DETAIL INFORMATION Page [4] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1. Pollutan CO	t Emitted:	2. Total Percent Efficiency of Control:		
3. Potentia	l Emissions:		4. Synth	netically Limited?
	11.91 lb/hour	tons/year	☐ Y	es √ No
5. Range o	f Estimated Fugitive Emissions (as	applicable):		
6. Emission	n Factor: 100 ppmdv, corrected to	$7\% O_2$		7. Emissions Method Code:
Referen	ce: PSD-FL-086(A)			0
8. Calculat	ion of Emissions:			
	by Florida permit PSD-FL-086(A)			
Limited	t Potential/Estimated Fugitive Emis by Florida permit PSD-FL-086(A), 5 lb/MMBtu. Facility-wide CO emi	which also con	ntains addi	

POLLUTANT DETAIL INFORMATION Page [5] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: HCL (H106)	2. Total Percent Effi	ciency of Control:
3.	Potential Emissions:	4. Sy	nthetically Limited?
	lb/hour 67.9	tons/year	Yes √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):	
6.	Emission Factor: 29 ppmdv or 95% remova	l, corrected to 7% O ₂	7. Emissions Method Code:
	Reference: PSD-FL-086(A)		0
8.	Calculation of Emissions:		i
	Limited by Florida permit PSD-FL-086(A)		
			•
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment:	
	Florida permit PSD-FL-086(A) limits HCL emissions to 29 ppmdv or 5 % of the potential sulfur dioxide emission (95% reduction by weight or volume), corrected to 7% O ₂ , whichever is less stringent.		

POLLUTANT DETAIL INFORMATION
Page [6] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: H107 (Fluoride (as HF))	2. Total Percer	nt Efficie	ncy of Control:
3.	Potential Emissions:	4	4. Synth	etically Limited?
	1.5 lb/hour 6.57	tons/year		es √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor:			7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:			
	Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment:		
	Limited by Florida permit PSD-FL-086(A), of 0.0125 lb/MMBtu.	which also conta	ains addit	ional emission limit

POLLUTANT DETAIL INFORMATION Page [7] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: PB	2. Total Percent Effic	iency of Control:
3.	Potential Emissions:	4. Syn	thetically Limited?
	0.0451 lb/hour 0.197	tons/year	Yes √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):	
6.	Emission Factor: 0.44 mg/dscm, corrected to	to 7% O ₂	7. Emissions Method Code:
	Reference: PSD-FL-086(A)		0
8.	Calculation of Emissions:		
0	Limited by Florida permit PSD-FL-086(A) Pollutant Potential/Estimated Eugitive Emis	sions Comment:	
9.	Pollutant Potential/Estimated Fugitive Emis Limited by Florida permit PSD-FL-086(A), of 3.76E-04 lb/MMBtu.		litional emission limit

POLLUTANT DETAIL INFORMATION Page [8] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

Pollutant Emitted:	2. Total Percent Efficiency of Control:	
H021 (Beryllium Compounds)		·
Potential Emissions:	4. Synth	netically Limited?
0.000115 lb/hour 5.04E-04	tons/year	res √ No
Range of Estimated Fugitive Emissions (as	applicable):	
·		
Emission Factor:		7. Emissions
		Method Code:
		0
Calculation of Emissions:		
YI I II TI II DOD TI OCCIO		
Limited by Florida permit PSD-FL-086(A)		
Pollutant Potential/Estimated Fugitive Emis	sions Comment:	
	which also contains addi	tional emission limit
of 9.58E-07 lb/MMBtu.		
	Potential Emissions: 0.000115 lb/hour 5.04E-04 Range of Estimated Fugitive Emissions (as Emission Factor: Reference: PSD-FL-086(A) Calculation of Emissions: Limited by Florida permit PSD-FL-086(A) Pollutant Potential/Estimated Fugitive Emis	Potential Emissions: 0.000115 lb/hour 5.04E-04 tons/year 4. Synth 0.000115 lb/hour 5.04E-04 tons/year

POLLUTANT DETAIL INFORMATION Page [9] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: H114 (Mercury Compounds)	2. Total Perce	ent Efficie	ency of Control:
3.	Potential Emissions: lb/hour 0.0605	tons/year	-	etically Limited? fes √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 0.070 mg/dscm or 85% re 7% O ₂	duction, correct	ted to	7. Emissions Method Code: 0
	Reference: PSD-FL-086(A)			
8.	Calculation of Emissions: Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment	•	
	Florida permit PSD-FL-086(A) limits H114 potential mercury emission concentration (8 to 7% O ₂ , whichever is less stringent.		_	

POLLUTANT DETAIL INFORMATION
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F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: DIOX	2. Total Perce	ent Efficie	ency of Control:
3.	Potential Emissions: 3.07E-06 lb/hour 1.35E-05	5 tons/year	•	etically Limited? es √ No
				C3 V 140
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 30 ng/dscm (total mass), o	corrected to 7%	O_2	7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:	·		
	Y : 11 FI :1			
	Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment	·•	
ا ک	1 official 1 official/Estimated Fugitive Emis	Sions Comment	••	
	Limited by Florida permit PSD-FL-086(A), of 2.56E-08 lb/MMBtu.	which also con	tains addit	tional emission limit

POLLUTANT DETAIL INFORMATION
Page [11] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: H027 (Cadmium Compounds)	2. Total Percent Effi	ciency of Control:
3.	Potential Emissions: 4.10E-03 lb/hour 0.0179	tons/year 4. Syn	nthetically Limited? Yes √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):	
6.	Emission Factor: 0.040 mg/dscm, corrected Reference: PSD-FL-086(A)	to 7% O ₂	7. Emissions Method Code: 0
8.	Calculation of Emissions:		
	Limited by Florida permit PSD-FL-086(A)		
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment:	
	Limited by Florida permit PSD-FL-086(A), of 3.42E-05 lb/MMBtu.	which also contains ad	ditional emission limit

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 1 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units: 27 mg/dscm, corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 2.76 lb/hour 12.1 ton	s/year
5.	Method of Compliance: Compliance with PM emission limits will be den 5.	nons	trated annually using EPA Reference	Method
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A)	Oper	ating Method):	

Allowable Emissions Allowable Emissions 2 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Emissions:	Allowable
3.	Allowable Emissions and Units: 29 ppmdv or 75% removal, corrected to 7% O ₂	4.	Equivalent Allowable En lb/hour	missions: tons/year
5.	Method of Compliance: Compliance with SO ₂ emission limits will be der Method 19 to calculate the daily geometric avera		_	PA Reference
6.	Allowable Emissions Comment (Description of C Florida permit PSD-FL-086(A) limits SO ₂ emiss dioxide emission (75% reduction by weight or vo stringent. Facility-wide SO ₂ emissions limited to	ions olum	to 29 ppmdv or 25 % of the), corrected to $7\% O_2$, where O_2 is the state of O_2 in O_2 in O_2 in O_2 in O_3 in $O_$	

Allowable Emissions 3 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Emissions:	Allowable
3.	Allowable Emissions and Units: 205 ppmdv, corrected to 7% O ₂	4.	Equivalent Allowable E 40.1 lb/hour	missions: tons/year
5.	Method of Compliance: Compliance with NO _X emission limits will be de Method 19 to calculate the daily arithmetic avera		strated via CEMS using I	
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A). Facil	•	•	ted to 679 tons/year.

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions 4 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 100 ppmdv, corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 11.9 lb/hour tons/year
5.	Method of Compliance: Compliance with CO emission limits will be demayerage.	nons	rated via CEMS using a 4-hour block
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A). Fac		

Allowable Emissions 5 of 11

1	. Basis for Allowable Emissions Code: RULE	2.	Future Effective Date Emissions:	e of Allowable
3	Allowable Emissions and Units: 29 ppmdv or 95% removal, corrected to 7% O ₂	4.	Equivalent Allowable lb/hour	e Emissions: 67.9 tons/year
5	 Method of Compliance: Compliance with HCL emission limits will be de Method 26 or 26A. 	emor	strated annually using	EPA Reference
6	Allowable Emissions Comment (Description of Comment PSD-FL-086(A) limits HCL emis dioxide emission (95% reduction by weight or vostringent.	sion	s to 29 ppmdv or 5 % o	

Allowable Emissions Allowable Emissions 6 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 1.5 lb/hour	4.	Equivalent Allowable Emissions: 6.57 tons/year
5.	Method of Compliance: Compliance with H107 (Fluoride (as HF)) emiss EPA Reference Method 13A or 13B.	on l	mits will be demonstrated every 5 years using
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A), whic 0.0125 lb/MMBtu.		

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 7 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 0.44 mg/dscm, corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 0.0451 lb/hour 0.197 tons/year
5.	Method of Compliance: Compliance with PB emission limits will be dem 29.	onst	rated annually using EPA Reference Method
6.	Allowable Emissions Comment (Description of Climited by Florida permit PSD-FL-086(A), which 3.76E-04 lb/MMBtu.		

Allowable Emissions 8 of 11

		_	
1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 0.000115 lb/hour	4.	Equivalent Allowable Emissions: 5.04E-04 tons/year
5.	Method of Compliance: Compliance with H021 (Beryllium Compounds) years using EPA Reference Method 29.	emi	ssion limits will be demonstrated every 5
6.	Allowable Emissions Comment (Description of CLimited by Florida permit PSD-FL-086(A), which 9.58E-07 lb/MMBtu.		

Allowable Emissions Allowable Emissions 9 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 0.070 mg/dscm or 85% removal, @ 7% O ₂	4.	Equivalent Allowable Emissions: lb/hour 0.0605 tons/year
5.	Method of Compliance: Compliance with H114 (Mercury Compounds) e EPA Reference Method 29.	miss	ion limits will be demonstrated annually using
6.	Allowable Emissions Comment (Description of C Florida permit PSD-FL-086(A) limits H114 emis mercury emission concentration (85% reduction whichever is less stringent.	sion	s to 0.070 mg/dscm or 15 % of the potential

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 10 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 30 ng/dscm (total mass), corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 3.07E-06 lb/hour 1.35E-05 tons/year
5.	Method of Compliance: Compliance with DIOX emission limits will be of Method 23.	lemo	nstrated annually using EPA Reference
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A), whice 2.56E-08 lb/MMBtu.		

Allowable Emissions Allowable Emissions 11 of 11

1.	Basis for Allowable Emissions Code: RULE	2. Future Effective Date of Allowable Emissions:		
3.	Allowable Emissions and Units: 0.040 mg/dscm, corrected to 7% O ₂	4. Equivalent Allowable Emissions: 4.10E-03 lb/hour, 3.42E-05 lb/MMBtu 0.0179 tons/year		
5.	Method of Compliance: Compliance with H027 (Cadmium Compounds) emission limits will be demonstrated annually using EPA Reference Method 29.			
6.	Allowable Emissions Comment (Description of Operating Method):			
	Limited by Florida permit PSD-FL-086(A)			

G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

<u>Visible Emissions Limitation:</u> Visible Emissions Limitation <u>1</u> of <u>1</u>

1.	Visible Emissions Subtype: VE	2. Basis for Allowable Opacity: √ Rule
3.	Allowable Opacity: Normal Conditions: 10 % Ex Maximum Period of Excess Opacity Allower	ceptional Conditions: 100 % ed: 3 hours
4.	Method of Compliance: EPA Reference Method 9 shall be used for except as provided under 40 CFR 60.11(e).	determining compliance with the opacity limit,
5.	Visible Emissions Comment: Excess emissions are allowed during startup duration of these events does not exceed 3 h	o, shut-down or malfunction, provided that the lours (40 CFR 60.56(b)).
Vis	sible Emissions Limitation: Visible Emissi	ons Limitation of
1.	Visible Emissions Subtype:	2. Basis for Allowable Opacity: Rule Other
	Allowable Opacity:	Rule Other ceptional Conditions: %
3.	Allowable Opacity: Normal Conditions: % Ex	Rule Other ceptional Conditions: %

H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

Continuous Monitoring System: Continuous Monitor $\underline{1}$ of $\underline{3}$

1.	Parameter Code: VE	Pollutant(s): Visible Emissions (Opacity)
3.	CMS Requirement:	
4.	Monitor Information Manufacturer: Land Model Number: 4500 MK II +	Serial Number: 0095471
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
	Monitor located at Fabric Filter outlet	
<u>Co</u>	ontinuous Monitoring System: Continuous	Monitor $\underline{2}$ of $\underline{3}$
1.	Parameter Code: EM, TEMP, FLOW	2. Pollutant(s): SO ₂ , O2, Temperature, Steam Flow
3.	CMS Requirement:	√ Rule
4.	Monitor Information Manufacturer: Sick	
	Model Number: MCS100EHW	Serial Number: 185
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
	Monitor located at SDA inlet	

H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

Continuous Monitoring System: Continuous Monitor 3 of 3

1.	Parameter Code:	2.	Pollutan	t(s):		
	EM			O _x , CO, SO ₂ , Temperature,		
			Steam F	low		
		√ R	ule	☐ Other		
4.	Monitor Information					
	Manufacturer: Sick					
	Model Number: MCS100EHW		Serial N	umber: 195		
5.	Installation Date:	6.	Perform	ance Specification Test Date:		
7.	Continuous Monitor Comment:					
	Monitor located at Fabric Filter outlet					
L	• •					
<u>Co</u>	ontinuous Monitoring System: Continuous Mo	onitor	r_of_			
1.	Parameter Code:	2.	Pollutar	at(s):		
3.	CMS Requirement:] Ru	ile	Other		
4.	Monitor Information Manufacturer:					
	Model Number:		Serial N	umber:		
5.	Installation Date:	6.	Perform	ance Specification Test Date:		
7.	Continuous Monitor Comment:					
′`	Continuous ratinos Comment.					

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 2 Previously Submitted, Date
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 8 Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 9 Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 10 Previously Submitted, Date
	☐ Not Applicable (construction application)
5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 11 Previously Submitted, Date Not Applicable
6.	Compliance Demonstration Reports/Records Attached, Document ID:
	Test Date(s)/Pollutant(s) Tested:
	Previously Submitted, Date: November 18, 2005
	Test Date(s)/Pollutant(s) Tested: 2005 compliance testing results and 2004 Statement of Compliance are included in Exhibit 12. To be Submitted, Date (if known):
	Test Date(s)/Pollutant(s) Tested: Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute Attached, Document ID: Not Applicable

Additional Requirements for Air Construction Permit Applications

	C 15 1 1 D : 14 1 : /	D 1 (0.010.400/6) 1 (0.010.500/5)
1.	Control Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7),
	F.A.C.; 40 CFR 63.43(d) and (e))	
	Attached, Document ID:	V Not Applicable
2.	Good Engineering Practice Stack Height An	alysis (Rule 62-212.400(5)(h)6., F.A.C., and
	Rule 62-212.500(4)(f), F.A.C.)	
	Attached, Document ID:	√ Not Applicable
3.	Description of Stack Sampling Facilities (R	equired for proposed new stack sampling
	facilities only)	
	Attached, Document ID:	√ Not Applicable
Ad	Iditional Requirements for Title V Air Ope	eration Permit Applications
1.	Identification of Applicable Requirements	-
	✓ Attached, Document ID: Exhibit 5	
2 (Compliance Assurance Monitoring	-
2. \	✓ Attached, Document ID: Exhibit 6	☐ Not Applicable
2		
3.	Alternative Methods of Operation	Mot Applicable
	Attached, Document ID:	√ Not Applicable
4.	Alternative Modes of Operation (Emissions	
	Attached, Document ID:	V Not Applicable
5.	Acid Rain Part Application	
	Certificate of Representation (EPA Form	n No. 7610-1)
	Copy Attached, Document ID:	
	Acid Rain Part (Form No. 62-210.900(1))(a))
	Attached, Document ID:	
	Previously Submitted, Date:	
	Repowering Extension Plan (Form No.	62-210.900(1)(a)1.)
	Attached, Document ID:	
	Previously Submitted, Date:	
	New Unit Exemption (Form No. 62-210.	900(1)(a)2.)
	Attached, Document ID:	
	Previously Submitted, Date:	
	Retired Unit Exemption (Form No. 62-2	
	Attached, Document ID:	<u> </u>
	Previously Submitted, Date:	
	Phase II NOx Compliance Plan (Form N	
	Attached, Document ID:	
	Previously Submitted, Date:	
	Phase II NOx Averaging Plan (Form No	
	Attached, Document ID:	
	Previously Submitted, Date:	
	√ Not Applicable	

Additional Requirements Comment
None

A. GENERAL EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Emissions Unit Classification

1.	Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)									
	 ✓ The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit. ✓ The emissions unit addressed in this Emissions Unit Information Section is an 									
	unregulated emissions unit.									
<u>En</u>	nissions Unit	Description and Sta	<u>ıtus</u>							
1.	 Type of Emissions Unit Addressed in this Section: (Check one) This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent). This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions. 									
		ssions Unit Informat cess or production ur								
2.	-	of Emissions Unit Advantage Taste Combustor & A								
3.	Emissions Un	nit Identification Nui	mbe	r: 106						
4.	4. Emissions Unit Status Construction Code: A									
9.	•	t: r: D.B. Riley			Mo	del Number: 276	0			
10	. Generator N	lameplate Rating: 2	2.5	MW						
11	duration of th	nit Comment: sions are allowed dur nese events does not malfunction period i	exc	eed 3 hours	per	occurrence. For	CO.	compliance, the		

Emissions Unit Control Equipment

1.	Control Equipment/Method(s) Description:							
	This emissions unit is equipped with a spray dryer absorber (SDA), activated carbon							
	injection system, fabric filter baghouse, and selective non-catalytic reduction (SNCR).							
1								
2.	Control Device or Method Code(s): 016, 048, 067, 107							
۷.	Control Device of Patentou Couc(s). 010, 040, 007, 107							

B. EMISSIONS UNIT CAPACITY INFORMATION

(Optional for unregulated emissions units.)

Emissions Unit Operating Capacity and Schedule

1.	Maximum Process or Throughput Rate:	
2.	Maximum Production Rate:	-
3.	Maximum Heat Input Rate: 120 MMBtu/hr (see item 6)	
4.	Maximum Incineration Rate:	
	288 tons/day	
5.	Requested Maximum Operating Schedule:	- -
	24 hours/day	7 days/week
	52 weeks/year	8,760 hours/year
6.	Operating Capacity/Schedule Comment:	
	120 MMBtu heat input rate for informational purposes only, not for Maximum steam flow and nominal capacity are limited by Florida p 086(A).	-

C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

Emission Point Description and Type

1.	1. Identification of Point on Plot Plan or Flow Diagram: See Exhibit 1		2. Emission Point Type Code: 1						
3.	3. Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking:								
	Not Applicable								
4.	ID Numbers or Descriptio	ns of Emission Ur	nits with this Emission	n Point in Common:					
	Not Applicable		•						
5.	Discharge Type Code: V	6. Stack Height 201 feet	:	7. Exit Diameter: 4.2 feet					
8.	Exit Temperature:		metric Flow Rate:	10. Water Vapor:					
0.	315°F	60,894 acfm		20% ±					
11.	Maximum Dry Standard F 36,686 dscfm	Flow Rate:	12. Nonstack Emission Point Height:						
13.	Emission Point UTM Coo Zone: 17 East (km):	ordinates 360.0	14. Emission Point Latitude/Longitude Latitude (DD/MM/SS)						
	North (km)	: 3091.9	Longitude (DD/I	MM/SS)					
15.	Emission Point Comment	:							
	Four MWCs have separate	e stacks (flues) loc	cated within a common	n enclosure.					
				·					

D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment Description and Rate: Segment 1 of 2

1.	Segment Description (Process/Fuel Type):								
	Solid Waste Disposal – Government Municipal Incineration – Stationary Mass Burn Waterwall Combustor								
2.	Source Classification Cod	e (SCC):	3. SCC Units:						
	50100105		Tons Burne	ed (all solid fuels)					
4.	Maximum Hourly Rate: See item 10	5. Maximum Annual Rate: See item 10		6.	Estimated Annual Activity Factor:				
7.	Maximum % Sulfur: N/A	8. Maximum % Ash: N/A		9.	Million Btu per SCC Unit: 10±				
10	10. Segment Comment: PSD-FL-086(A) limits nominal heat input to 104 MMBtu/hr and nominal capacity to 250 tons per day (rolling 12-month average).								

Segment Description and Rate: Segment 2 of 2

30	Segment Description and Nate. Segment 2 of 2								
1.	Segment Description (Process/Fuel Type):								
	Solid Waste Disposal – Government Auxiliary Fuel/No Emissions – Natural Gas								
2.	Source Classification Cod	e (S	CC):	3.	SCC Units	:			
1	50190006			Million Cubic Feet Burned (all gaseous					
					fuels)				
4.	Maximum Hourly Rate: See item 10	5.	Maximum .	Ann	ual Rate:	6.	Estimated Annual Activity Factor:		
7.	Maximum % Sulfur:	8.	Maximum	% A	sh:	9.	Million Btu per SCC Unit:		
	N/A		N/A				1,027±		
10	10. Segment Comment:								
	PSD-FL-086(A) limits the	ma	ximum hourl	y ra	ate by the 10°	% an	mual capacity factor.		

E. EMISSIONS UNIT POLLUTANTS

List of Pollutants Emitted by Emissions Unit

1. Pollutant Emitted	2. Primary Control	3. Secondary Control	4. Pollutant
	Device Code	Device Code	Regulatory Code
PM	016		EL
SO2	067	016	EL
NOX	107		EL
СО			EL
HCL (H106)	067	016	EL
H107	016		EL
PB	016		EL
H021	016		EL
H114	048		EL
DIOX	067	016	EL
H027	016		EL
			-

POLLUTANT DETAIL INFORMATION
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F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: PM	2. Total Perce	ent Efficie	ency of Control:
3.	Potential Emissions: 2.76 lb/hour 12.3	l tons/year	•	etically Limited? fes √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 27 mg/dscm, corrected to	7% O ₂		7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions: Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment	:	
	Limited by Florida permit PSD-FL-086(A)			

POLLUTANT DETAIL INFORMATION Page [2] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: SO2	2. Total Perc	ent Efficie	ency of Control:
3.	Potential Emissions:		4. Synth	etically Limited?
	lb/hour	tons/year	□ Y	es √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 29 ppmdv or 75% remova	al, corrected to	7% O ₂	7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:			
0	Limited by Florida permit PSD-FL-086(A)		4.	
9.	Pollutant Potential/Estimated Fugitive Emis	sions Commen	t:	
	Florida permit PSD-FL-086(A) limits SO ₂ emissions to 29 ppmdv or 25 % of the potential sulfur dioxide emission (75% reduction by weight or volume), corrected to 7% O ₂ , whichever is less stringent. Facility-wide SO ₂ emissions limited to 460 tons/year.			

POLLUTANT DETAIL INFORMATION
Page [3] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

Pollutant Emitted: NOX	2. Total Percent Eff	iciency of Control:
3. Potential Emissions: 40.1 lb/hour	tons/year 4. Sy	ynthetically Limited?] Yes √ No
5. Range of Estimated Fugitive Emissions (as	applicable):	
6. Emission Factor: 205 ppmdv, corrected to Reference: PSD-FL-086(A)	7% O₂	7. Emissions Method Code: 0
8. Calculation of Emissions:		<u> </u>
Limited by Florida permit PSD-FL-086(A) 9. Pollutant Potential/Estimated Fugitive Emis		
 Pollutant Potential/Estimated Fugitive Emissions Comment: Limited by Florida permit PSD-FL-086(A), which also contains additional emission limit of 0.335 lb/MMBtu. Facility-wide NO_X emissions limited to 679 tons/year. 		

POLLUTANT DETAIL INFORMATION
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F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted:	2. Total Pero	ent Efficie	ency of Control:
3.	Potential Emissions: 11.91 lb/hour	tons/year		netically Limited? Yes √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 100 ppmdv, corrected to 7 Reference: PSD-FL-086(A)	7% O₂		7. Emissions Method Code: 0
8.	Calculation of Emissions:			
	Limited by Florida permit PSD-FL-086(A)			
9.	 Pollutant Potential/Estimated Fugitive Emissions Comment: Limited by Florida permit PSD-FL-086(A), which also contains additional emission limit of 0.0995 lb/MMBtu. Facility-wide CO emissions limited to 185 tons/year. 			

POLLUTANT DETAIL INFORMATION
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F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: HCL (H106)	2. Total Perce	ent Efficie	ncy of Control:
3.	Potential Emissions:		4. Synth	etically Limited?
	lb/hour 67.9	tons/year		es √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 29 ppmdv or 95% remova	l, corrected to 7	% O ₂	7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:			
0	Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment:	:	
	Florida permit PSD-FL-086(A) limits HCL emissions to 29 ppmdv or 5 % of the potential sulfur dioxide emission (95% reduction by weight or volume), corrected to 7% O_2 , whichever is less stringent.			

POLLUTANT DETAIL INFORMATION Page [6] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: H107 (Fluoride (as HF))	2. Total Percent	Efficie	ncy of Control:
3.	Potential Emissions:	4.	Synth	etically Limited?
	1.5 lb/hour 6.57	tons/year	Y	es √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor:			7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:			
	Limited by Florida permit PSD-FL-086(A)			
		·		
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment:		
	Limited by Florida permit PSD-FL-086(A), which also contains additional emission limit of 0.0125 lb/MMBtu.			

POLLUTANT DETAIL INFORMATION
Page [7] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted: PB	2. Total Percent Efficie	ency of Control:
3.	Potential Emissions: 0.0451 lb/hour 0.197		tetically Limited? Tes √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):	
6.	Emission Factor: 0.44 mg/dscm, corrected t	to 7% O ₂	7. Emissions Method Code:
	Reference: PSD-FL-086(A)		0
8.	Calculation of Emissions: Limited by Florida permit PSD-FL-086(A)		
9.	Pollutant Potential/Estimated Fugitive Emis Limited by Florida permit PSD-FL-086(A), of 3.76E-04 lb/MMBtu.		tional emission limit

POLLUTANT DETAIL INFORMATION
Page [8] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

1.	Pollutant Emitted:	2. Total Percent Efficiency of Control:
	H021 (Beryllium Compounds)	
3.	Potential Emissions:	4. Synthetically Limited?
	0.000115 lb/hour 5.04E-04	tons/year Yes V No
5.	Range of Estimated Fugitive Emissions (as	applicable):
6.	Emission Factor:	7. Emissions
		Method Code:
	Reference: PSD-FL-086(A)	0
8.	Calculation of Emissions:	
	Limited by Florida permit PSD-FL-086(A)	
	•	
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment:
	•	which also contains additional emission limit
	of 9.58E-07 lb/MMBtu.	

EMISSIONS UNIT INFORMATION Section [7] of [8]

POLLUTANT DETAIL INFORMATION
Page [9] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted:	2. Total Perc	ent Efficie	ency of Control:
	H114 (Mercury Compounds)			
3.	Potential Emissions:		4. Synth	etically Limited?
	lb/hour 0.0603	5 tons/year	□ Y	es √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 0.070 mg/dscm or 85% re 7% O ₂	eduction, correc	ted to	7. Emissions Method Code: 0
	Reference: PSD-FL-086(A)			
8.	Calculation of Emissions:			
	Limited by Florida permit PSD-FL-086(A)			
				•
9.	Pollutant Potential/Estimated Fugitive Emis	sions Commen	t:	
	Florida permit PSD-FL-086(A) limits H114 potential mercury emission concentration (8 to 7% O ₂ , whichever is less stringent.		_	

EMISSIONS UNIT INFORMATION Section [7] of [8]

POLLUTANT DETAIL INFORMATION Page [10] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted: DIOX	2. Total Percer	nt Efficie	ncy of Control:
3.	Potential Emissions: 3.07E-06 lb/hour 1.35E-05		•	etically Limited? es No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
6.	Emission Factor: 30 ng/dscm (total mass), of	corrected to 7% (O_2	7. Emissions Method Code:
	Reference: PSD-FL-086(A)			0
8.	Calculation of Emissions:			
	Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis Limited by Florida permit PSD-FL-086(A), of 2.56E-08 lb/MMBtu.			ional emission limit

POLLUTANT DETAIL INFORMATION
Page [11] of [11]

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted: H027 (Cadmium Compounds)	2. Total Perce	ent Efficie	ency of Control:
3.	Potential Emissions:	tons/year	•	netically Limited? Tes √ No
5.	Range of Estimated Fugitive Emissions (as	applicable):	_	·
6.	Emission Factor: 0.040 mg/dscm, corrected Reference: PSD-FL-086(A)	l to 7% O ₂		7. Emissions Method Code: 0
8.	Calculation of Emissions:		<u>-</u>	
	Limited by Florida permit PSD-FL-086(A)			
9.	Pollutant Potential/Estimated Fugitive Emis	sions Comment	:	
	Limited by Florida permit PSD-FL-086(A), of 3.42E-05 lb/MMBtu.	which also con	tains addit	tional emission limit
L				

POLLUTANT DETAIL INFORMATION Page [1] of [4]

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 1 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Emissions:	Allowable
3.	Allowable Emissions and Units: 27 mg/dscm, corrected to 7% O ₂	4.	Equivalent Allowable E 2.76 lb/hour	missions: 12.1 tons/year
5.	Method of Compliance: Compliance with PM emission limits will be demonstrated annually using EPA Reference Method 5.			
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A)	Oper	ating Method):	

Allowable Emissions 2 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date Emissions:	e of Allowable	
3.	Allowable Emissions and Units: 29 ppmdv or 75% removal, corrected to 7% O ₂	4.	Equivalent Allowable	Emissions: tons/year	
5.	Method of Compliance: Compliance with SO ₂ emission limits will be demonstrated via CEMS using EPA Reference Method 19 to calculate the daily geometric average SO ₂ concentration.				
6.	Allowable Emissions Comment (Description of Operating Method): Florida permit PSD-FL-086(A) limits SO ₂ emissions to 29 ppmdv or 25 % of the potential sulfur dioxide emission (75% reduction by weight or volume), corrected to 7% O ₂ , whichever is less stringent. Facility-wide SO ₂ emissions limited to 460 tons/year.				

Allowable Emissions 3 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units: 205 ppmdv, corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 40.1 lb/hour tons/year	
5.	Method of Compliance: Compliance with NO _X emission limits will be demonstrated via CEMS using EPA Reference Method 19 to calculate the daily arithmetic average NO _X concentration.			
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A). Facil	•	•	

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 4 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units: 100 ppmdv, corrected to 7% O ₂	4.	Equivalent Allowable Emissions: 11.9 lb/hour tons/year	
5.	Method of Compliance: Compliance with CO emission limits will be demonstrated via CEMS using a 4-hour block average.			
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A). Fac			

Allowable Emissions 5 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Emissions:	f Allowable
3.		4.	Equivalent Allowable I	
	29 ppmdv or 95% removal, corrected to 7% O ₂		lb/hour	67.9 tons/year
5.	Method of Compliance: Compliance with HCL emission limits will be demonstrated annually using EPA Reference Method 26 or 26A.			
6.	Allowable Emissions Comment (Description of C Florida permit PSD-FL-086(A) limits HCL emis dioxide emission (95% reduction by weight or vo stringent.	sion	s to 29 ppmdv or 5 % of	-

Allowable Emissions Allowable Emissions 6 of 11

1.	Basis for Allowable Emissions Code: RULE	Future Effective Date of Allowable Emissions:		
3.	Allowable Emissions and Units: 1.5 lb/hour	4. Equivalent Allowable Emissions: 6.57 tons/year		
5.	. Method of Compliance: Compliance with H107 (Fluoride (as HF)) emission limits will be demonstrated every 5 years using EPA Reference Method 13A or 13B.			
6.	Allowable Emissions Comment (Description of Limited by Florida permit PSD-FL-086(A), which 0.0125 lb/MMBtu.			

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 7 of 11

1.	Basis for Allowable Emissions Code: RULE	Future Effective Date of Allowable Emissions:			
3.	Allowable Emissions and Units: 0.44 mg/dscm, corrected to 7% O ₂	4. Equivalent Allowable Emissions: 0.0451 lb/hour 0.197 tons/year			
5.	. Method of Compliance: Compliance with PB emission limits will be demonstrated annually using EPA Reference Method 29.				
6.					

Allowable Emissions 8 of 11

1.	Basis for Allowable Emissions Code: RULE	l	Future Effective Date of Allowable Emissions:		
3.	Allowable Emissions and Units: 0.000115 lb/hour	4.	Equivalent Allowable Emissions: 5.04E-04 tons/year		
5.	5. Method of Compliance: Compliance with H021 (Beryllium Compounds) emission limits will be demonstrated every 5 years using EPA Reference Method 29.				
6.	Allowable Emissions Comment (Description of C Limited by Florida permit PSD-FL-086(A), whice 9.58E-07 lb/MMBtu.		<u> </u>		

Allowable Emissions Allowable Emissions 9 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 0.070 mg/dscm or 85% removal, @ 7% O ₂	4.	Equivalent Allowable Emissions: 1b/hour 0.0605 tons/year
5.	Method of Compliance: Compliance with H114 (Mercury Compounds) emission limits will be demonstrated annually using EPA Reference Method 29.		
6.	Allowable Emissions Comment (Description of Florida permit PSD-FL-086(A) limits H114 emismercury emission concentration (85% reduction whichever is less stringent.	ssion	s to 0.070 mg/dscm or 15 % of the potential

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 10 of 11

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	3. Allowable Emissions and Units: 30 ng/dscm (total mass), corrected to 7% O ₂		Equivalent Allowable Emissions: 3.07E-06 lb/hour 1.35E-05 tons/year
5.	. Method of Compliance: Compliance with DIOX emission limits will be demonstrated annually using EPA Reference Method 23.		
6.	6. Allowable Emissions Comment (Description of Operating Method): Limited by Florida permit PSD-FL-086(A), which also contains additional emission limit of 2.56E-08 lb/MMBtu.		

Allowable Emissions 11 of 11

1.	Basis for Allowable Emissions Code: RULE	2. Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units: 0.040 mg/dscm, corrected to 7% O ₂	4. Equivalent Allowable Emissions: 4.10E-03 lb/hour, 3.42E-05 lb/MMBtu 0.0179 tons/year	
5.	Method of Compliance: Compliance with H027 (Cadmium Compounds) emission limits will be demonstrated annually using EPA Reference Method 29.		
6.	Allowable Emissions Comment (Description of Operating Method): Limited by Florida permit PSD-FL-086(A)		
	Emilied by Fiorida permit 13D-FE-000(A)		

EMISSIONS UNIT INFORMATION Section [7] of [8]

G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

<u>Visible Emissions Limitation:</u> Visible Emissions Limitation <u>1</u> of <u>1</u>

1.	Visible Emissions Subtype: VE	2. Basis for Allowable Opacity: √ Rule ☐ Other	
3.	Allowable Opacity: Normal Conditions: 10 % Ex Maximum Period of Excess Opacity Allower	ceptional Conditions: 100 % a hours	
4.	Method of Compliance: EPA Reference Method 9 shall be used for except as provided under 40 CFR 60.11(e).	determining compliance with the opacity limi	it
5.	Visible Emissions Comment: Excess emissions are allowed during startup duration of these events does not exceed 3 h	o, shut-down or malfunction, provided that the lours (40 CFR 60.56(b)).	e
			,
Vi	sible Emissions Limitation: Visible Emissi	ons Limitation of	
	sible Emissions Limitation: Visible Emissi Visible Emissions Subtype:	ons Limitation of 2. Basis for Allowable Opacity: Rule Other	
1.	Visible Emissions Subtype: Allowable Opacity:	2. Basis for Allowable Opacity: Rule Other ceptional Conditions: %	
3.	Visible Emissions Subtype: Allowable Opacity: Normal Conditions: % Ex	2. Basis for Allowable Opacity: Rule Other ceptional Conditions: %	

H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

<u>Continuous Monitoring System:</u> Continuous Monitor <u>1</u> of <u>3</u>

1.	Parameter Code:	2. Pollutant(s):
	VE	Visible Emissions (Opacity)
	CMS Requirement:	√ Rule
4.	Monitor Information	
	Manufacturer: Land	
	Model Number: 4500	Serial Number: 9995456
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
	Monitor located at Fabric Filter outlet	
<u>Co</u>	ontinuous Monitoring System: Continuous	Monitor $\underline{2}$ of $\underline{3}$
1.	Parameter Code:	2. Pollutant(s):
	EM, TEMP, FLOW	SO ₂ , O ₂ , Temperature, Steam Flow
3.	CMS Requirement:	√ Rule
4.	Monitor Information Manufacturer: Sick	
		Carial Number 194
	Model Number: MCS100EHW	Serial Number: 184
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
	Monitor located at SDA inlet	

EMISSIONS UNIT INFORMATION Section [7] of [8]

H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

Continuous Monitoring System: Continuous Monitor 3 of 3

1.	Parameter Code:	2. Pollutant(s):
	EM, TEMP, FLOW	O ₂ , NO _X , CO, SO ₂ , Temperature,
		Steam Flow
3.	CMS Requirement:	Rule
4.	Monitor Information	
	Manufacturer: Sick	•
	Model Number: MCS100EHW	Serial Number: 194
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
	Monitor located at Fabric Filter outlet	
Co	entinuous Manitaring System: Continuous Ma	pritor of
	ontinuous Monitoring System: Continuous Mo	-
1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	Rule Other
4.	Monitor Information	-
	Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 2 Previously Submitted, Date
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 8 Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 9 Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 10 Previously Submitted, Date
	☐ Not Applicable (construction application)
5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 11 Previously Submitted, Date Not Applicable
6.	Compliance Demonstration Reports/Records Attached, Document ID:
	Test Date(s)/Pollutant(s) Tested:
	Previously Submitted, Date: November 18, 2005
	Test Date(s)/Pollutant(s) Tested: 2005 compliance testing results and 2004 Statement of Compliance are included in Exhibit 12.
	To be Submitted, Date (if known):
	Test Date(s)/Pollutant(s) Tested: Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute ☐ Attached, Document ID:

EMISSIONS UNIT INFORMATION

Section [7] **of** [8]

Additional Requirements for Air Construction Permit Applications

1.	Control Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7),
	F.A.C.; 40 CFR 63.43(d) and (e))
	Attached, Document ID: Not Applicable
2.	Good Engineering Practice Stack Height Analysis (Rule 62-212.400(5)(h)6., F.A.C., and Rule 62-212.500(4)(f), F.A.C.)
	Attached, Document ID: Not Applicable
3.	Description of Stack Sampling Facilities (Required for proposed new stack sampling
	facilities only) ☐ Attached, Document ID:
	Attached, Bocument ID V Not Applicable
<u>Ac</u>	Iditional Requirements for Title V Air Operation Permit Applications
1.	Identification of Applicable Requirements
	√ Attached, Document ID: Exhibit 5
2.	Compliance Assurance Monitoring
	✓ Attached, Document ID: Exhibit 6 Not Applicable
3.	Alternative Methods of Operation
	Attached, Document ID: V Not Applicable
4.	Alternative Modes of Operation (Emissions Trading)
	Attached, Document ID: Not Applicable
5.	Acid Rain Part Application
	Certificate of Representation (EPA Form No. 7610-1)
	Copy Attached, Document ID:
	Acid Rain Part (Form No. 62-210.900(1)(a))
	Attached, Document ID:
	Previously Submitted, Date:
	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
	Attached, Document ID:
	Previously Submitted, Date: New Unit Exemption (Form No. 62-210.900(1)(a)2.)
	Attached, Document ID:
	Previously Submitted, Date:
ļ	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)
	Attached, Document ID:
	Previously Submitted, Date:
	Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)
	Attached, Document ID:
	Previously Submitted, Date:
	Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)
	Attached, Document ID:
	Previously Submitted, Date:
	√ Not Applicable

EMISSIONS UNIT INFORMATION Section [7] of [8]

Additional Requirements Comment				
None				
			•	

EMISSIONS UNIT INFORMATION Section [8] of [8]

A. GENERAL EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Emissions Unit Classification

1.	Regulated or	Unregulated Emissic	ons Unit? (Che	ck one if annlying for	an initial revised or
1.	Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)				
	The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.				ection is a regulated
		sions unit addressed demissions unit.	in this Emissio	ons Unit Information S	ection is an
En	nissions Unit	Description and Sta	ıtu <u>s</u>		
1.	Type of Emis	ssions Unit Addresse	d in this Section	on: (Check one)	
	process o	r production unit, or	activity, which	dresses, as a single em a produces one or more int (stack or vent).	_
	which has at least one definable emission point (stack or vent). This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.				
	This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only.				
2.	. Description of Emissions Unit Addressed in this Section:				
	Cooling Tower				
3.	Emissions U	nit Identification Nu	mber: 107		
4.	Emissions	5. Commence	6. Initial	7. Emissions Unit	8. Acid Rain Unit?
	Unit Status	Construction	Startup	Major Group	Yes
	Code:	Date:	Date: 1985	SIC Code: 49	√ No
9.	Package Unit	<u>.</u> t:			
	Manufacturer: Marley Cooling Tower Co. Model Number: 597-58-2				
10.	10. Generator Nameplate Rating:				
11	. Emissions U	nit Comment:			
	None				
	None				

EMISSIONS UNIT INFORMATION Section [8] of [8]

Emissions Unit Control Equipment

Control Equipment/Method(s) Description:		
·		
2. Control Device or Method Code(s):		

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) V Attached, Document ID: Exhibit 2 Previously Submitted, Date
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 8 Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Exhibit 9 Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) V Attached, Document ID: Exhibit 10 Previously Submitted, Date
5.	 Not Applicable (construction application) Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) ✓ Attached, Document ID: Exhibit 11
6.	Compliance Demonstration Reports/Records Attached, Document ID: Test Date(s)/Pollutant(s) Tested:
	Previously Submitted, Date: Test Date(s)/Pollutant(s) Tested:
	To be Submitted, Date (if known): Test Date(s)/Pollutant(s) Tested:
	√ Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute Attached, Document ID: Not Applicable

EMISSIONS UNIT INFORMATION Section [8] of [8]

Additional Requirements for Air Construction Permit Applications

1. Control Technology Review and Ana	lysis (Rules 62-212.400(6) and 62-212.500(7),
F.A.C.; 40 CFR 63.43(d) and (e))	_
Attached, Document ID:	Not Applicable
, , ,	ght Analysis (Rule 62-212.400(5)(h)6., F.A.C., and
Rule 62-212.500(4)(f), F.A.C.)	_
Attached, Document ID:	
3. Description of Stack Sampling Facility facilities only)	ties (Required for proposed new stack sampling
Attached, Document ID:	✓ Not Applicable
L	
Additional Requirements for Title V A	
1. Identification of Applicable Requiren	
Attached, Document ID: Exhibit 5	<u>1</u>
2. Compliance Assurance Monitoring	
Attached, Document ID: Exhibit 6	Not Applicable
3. Alternative Methods of Operation	
Attached, Document ID:	Not Applicable
4. Alternative Modes of Operation (Emis	ssions Trading)
Attached, Document ID:	Not Applicable
5. Acid Rain Part Application	
☐ Certificate of Representation (EPA	A Form No. 7610-1)
Copy Attached, Document I	
☐ Acid Rain Part (Form No. 62-210	, , , , ,
Attached, Document ID:	
☐ Previously Submitted, Date:	
Repowering Extension Plan (Form	
Attached, Document ID:	
☐ Previously Submitted, Date:	······································
☐ New Unit Exemption (Form No. 6	52-210.900(1)(a)2.)
Attached, Document ID:	
☐ Previously Submitted, Date:	
☐ Retired Unit Exemption (Form No	
Attached, Document ID:	
☐ Previously Submitted, Date:	
☐ Phase II NOx Compliance Plan (F	Form No. 62-210.900(1)(a)4.)
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☐ Previously Submitted, Date:	·
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√ Not Applicable	

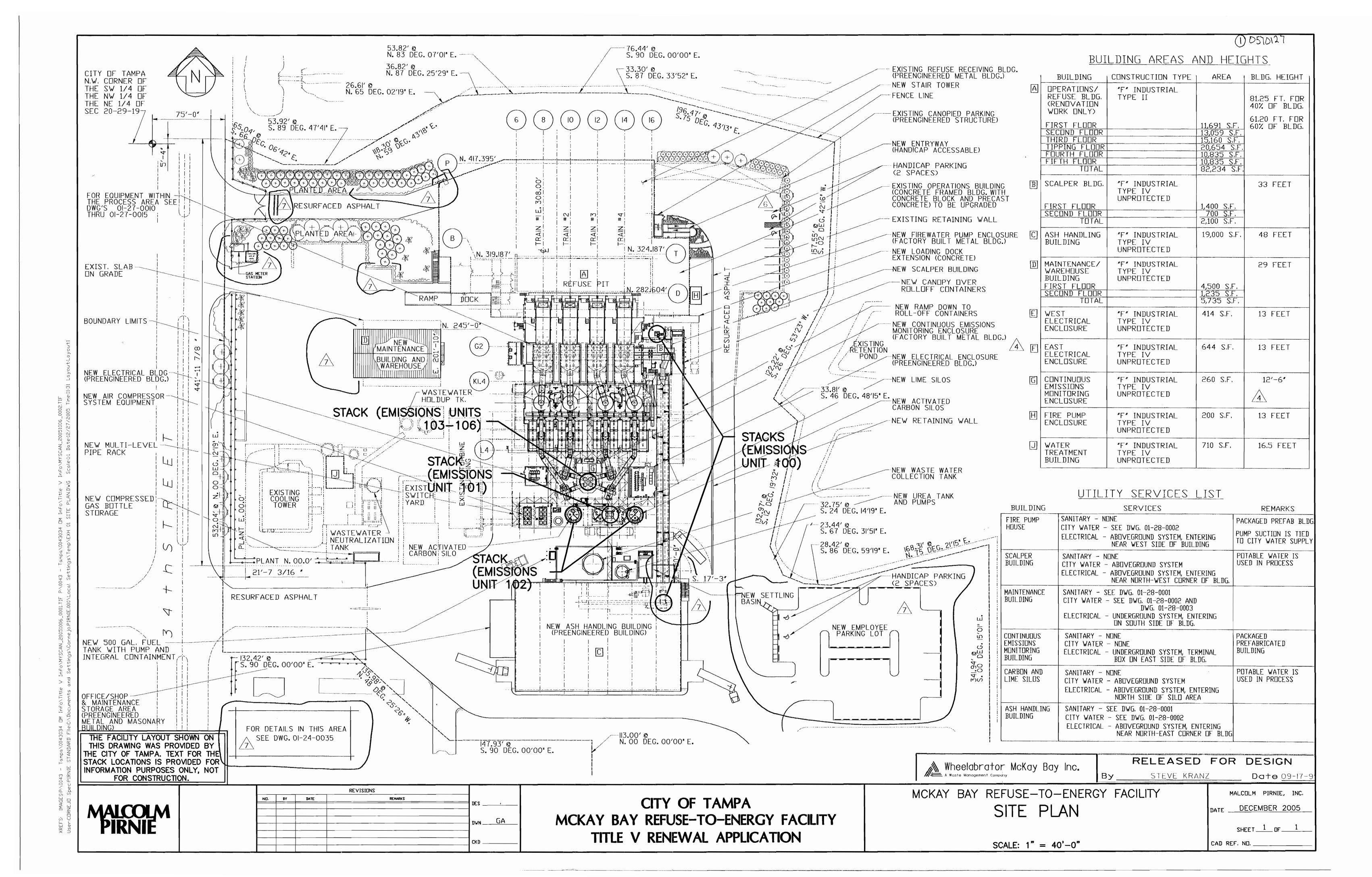
EMISSIONS UNIT INFORMATION Section [8] of [8] Additional Requirements Comment

None		



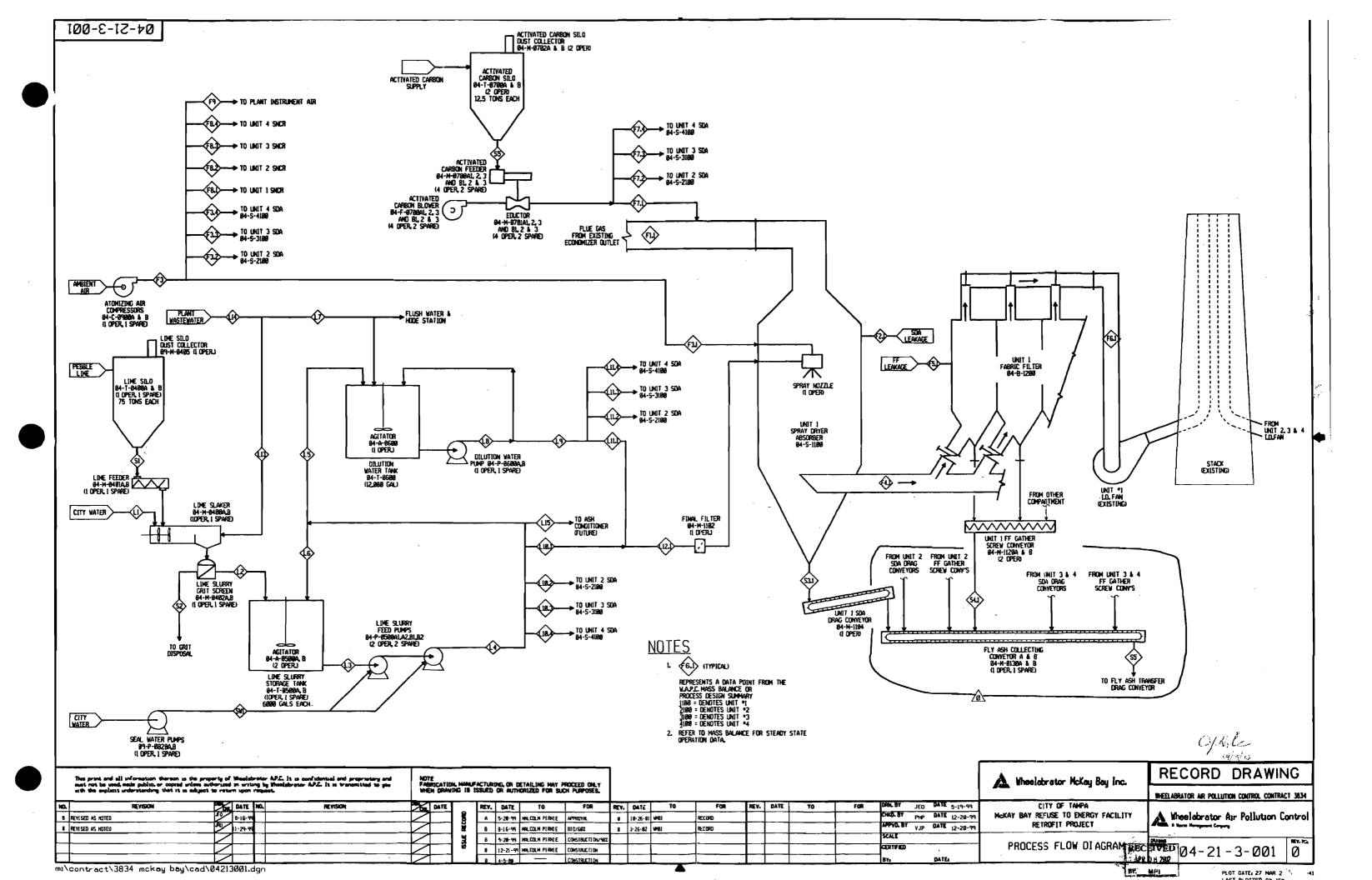
FACILITY ADDITIONAL INFORMATION ADDITIONAL REQUIREMENTS FOR ALL APPLICATIONS

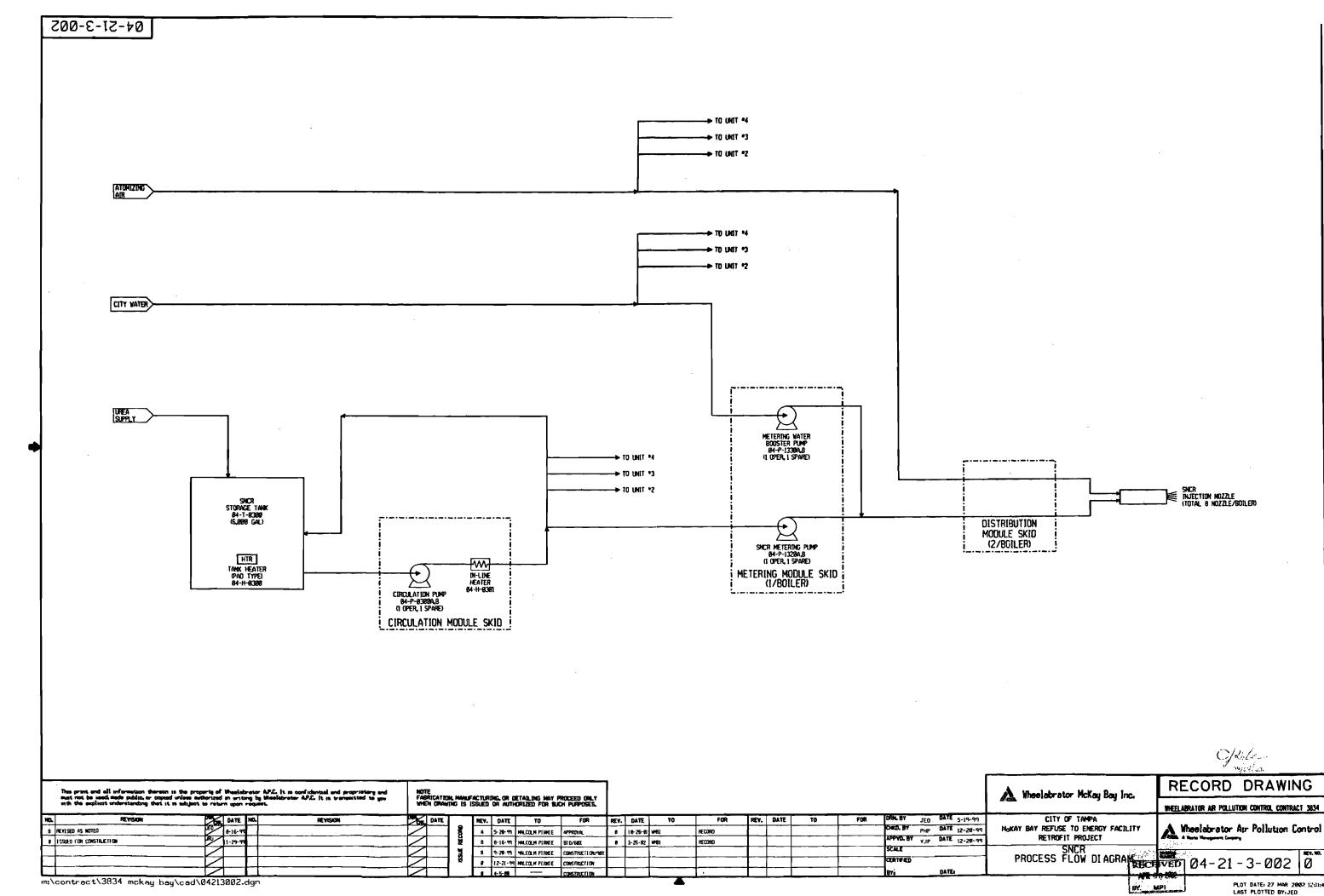
FACILITY PLOT PLAN





GENERAL PROCESS FLOW DIAGRAMS





PLOT DATE: 27 MAR 2002 12:11:44 LAST PLOTTED BY: JED

MALCOLM PIRNIE

PRECAUTIONS TO PREVENT EMISSIONS OF UNCONTROLLED PARTICULATE MATTER



PRECAUTIONS TO PREVENT EMISSIONS OF UNCONTROLLED PARTICULATE MATTER

Reasonable precautions used at the McKay Bay Refuse-To-Energy Facility (the "Facility") to prevent emissions of uncontrolled particulate matter include the following:

- Roads, parking areas, and yards are paved. A street sweeper equipped with a vacuum system is used to remove particulate matter from roads and other paved areas.
- The tipping floor is located in an enclosed building. Airflow to the boilers provides a negative draft in the tipping building, which minimizes emissions of particulate matter. Floors are washed as required by the Facility's solid waste permit.
- Unpaved areas of the Facility are maintained and either sodded or landscaped.
- Boiler ash and grate siftings are quenched and wetted. Ash conveyors and transfer points are enclosed and maintained to minimize fugitive emissions. Fly ash is wetted in a pug mill ash conditioning system and then blended with the wet boiler ash and grate siftings. The wetted combined ash is processed for recyclable ferrous metals and stored in a building prior to loading in a truck for disposal. The scalper building and ash management building are equipped with wet scrubbers to control fugitive emissions. Floors are washed as required by the Facility's solid waste permit. The ash hauling trucks are equipped with tarps.



FACILITY ADDITIONAL INFORMATION ADDITIONAL REQUIREMENTS FOR TITLE V AIR OPERATIONS PERMIT APPLICATIONS



LIST OF INSIGNIFICANT ACTIVITIES



LIST OF INSIGNIFICANT ACTIVITIES

The process or production units or other pollutant-emitting activities listed below are located on the Title V site addressed in this application and are, by virtue of size or operating rate, eligible for treatment as insignificant emission units in accordance with the criteria of Rule 62-213.430(6)(b), F.A.C., and are requested to be treated as such pursuant to Rule 62-213.420(3), F.A.C. Descriptions and emissions estimates (as necessary) for these insignificant activities/sources are included on the pages that follow.

Activity/Source	Estimated Emissions, Tons/Year				Comments	
71ctivity/oddiec	PM/PM10	NO_x	СО	$O \mid VOC \mid SO_2$		
Paint Usage (less than 6 gal/day)						Meets criteria of Rule 62-213.430(6)
Boiler and Cooling Tower Chemicals						Listed as trivial source in USEPA White Paper No. 1 (1995)
Solvent Degreaser						Meets criteria of Rule 62-213.430(6)
Urea Storage Tank						Meets criteria of Rule 62-213.430(6)
Caustic Soda Tank						Meets criteria of Rule 62-213.430(6)
Sulfuric Acid Tank						Meets criteria of Rule 62-213.430(6)
500 Gallon Diesel Fuel Storage Tank						Meets criteria of Rule 62-213.430(6)
Vehicular Traffic & Mobile on- site Eqipment						Meets criteria of Rule 62-213.430(6)
Refuse Pit						Meets criteria of Rule 62-213.430(6)
Emergency Generator	Engine emissions exempt under FAC 62-210.300(3)					
Portable Air Compressors	Negligible					Listed as trivial source in USEPA White Paper No. 1 (1995)
Portable Welding Machines	Negligible					Categorically exempt under Rule 62-210.300(3)(a)(21)
Fire & Safety Equipment						Meets criteria of Rule 62-213.430(6)
Sandblasting Equipment						Meets criteria of Rule 62-213.430(6)



Activity Descriptions and Emission Estimate Calculations

Paint Usage (less than 6.0 gal/day)

Paint usage associated with plant maintenance and upkeep activities satisfies the requirements of Rules 62-210.300(3)(a)(23) and 62-213.430(6)(b) and should be considered insignificant.

Boiler and Cooling Tower Chemicals

Chemicals used in boiler feedwater operations are listed as trivial in the *White Paper for Streamlined Development of Part 70 Permit Applications (EPA, 1995)* and should be considered insignificant.

Solvent Degreaser

The facility has a cold cleaner unit in the maintenance area. The degreasing unit satisfies the requirements of Rules 62-210.300(3)(a)(26) and 62-213.430(6)(b) and should be considered insignificant.

Caustic Soda Tank

The emissions activity associated with this tank meets the criteria of Rule 62-213.430(6)(b), F.A.C. and should be considered insignificant.

Sulfuric Acid Tank

The facility has one 5,000 gallon sulfuric acid tank on site for water treatment operations. The tank satisfies the requirements of Rule 62-213.430(6)(b) and should be considered insignificant.

Urea Storage Tank

The facility has one 6,000 gallon urea tank for the NO_x control system. The tank satisfies the requirements of Rule 62-213.430(6)(b) and should be considered insignificant.

MALCOLM PIRNIE

MCKAY BAY REFUSE-TO-ENERGY FACILITY TITLE V RENEWAL APPLICATION

Diesel Fuel Storage Tank

The Facility has one 500 gallon diesel fuel storage tank for refueling mobile on-site equipment and vehicles. The tank satisfies the requirements of Rules 62-210.300(3)(a)(34) and 62-213.430(6)(b) and should be considered insignificant.

Vehicular Traffic and Mobile On-Site Equipment

Combustion emissions from propulsion of mobile sources satisfies the requirements of Rule 62-213.430(6)(b) and should be considered insignificant.

Refuse Pit

Refuse pit emissions satisfy the requirements of Rule 62-213.430(6)(b) and should be considered insignificant.

Emergency Generator

The emergency generator satisfies the requirements of Rules 62-210.300(3)(a)(20) and 62-213.430(6)(b) F.A.C. and should be considered insignificant.

Portable Air Compressors

Air compressors and pneumatically operated equipment are listed as trivial in the *White Paper for Streamlined Development of Part 70 Permit Applications (EPA, 1995)* and should be considered insignificant.

Portable Welding Machines

The engines that power the welders satisfy the categorical exemption requirements for general-purpose internal combustion engines in Rule 62-210.300(3)(a)(21), F.A.C. and should be considered insignificant.

Fire & Safety Equipment

Fire and safety equipment are categorically exempt under Rule 62-210.300(3)(a)(22), F.A.C. and should be considered insignificant.



Sandblasting	Equipment
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Sandblasting equipment satisfies the requirements of Rule 62-213.430(6)(b) and should be considered insignificant.







LIST OF APPLICABLE REGULATIONS

FEDERAL REGULATIONS

- 40 CFR 50 Ambient Air Quality Standards
- 40 CFR 52 (All terms and conditions of Florida permit PSD-FL-086(A))
- 40 CFR 60, Subparts A, Cb, Db, E
- 40 CFR 61 National Emissions Standards for Hazardous Air Pollutants (NESHAP)
- 40 CFR 64 Compliance Assurance Monitoring Rule
- 40 CFR 82 Stratospheric Ozone Protection

FLORIDA ADMINISTRATIVE CODE

All terms & conditions of Florida Permit PSD-FL-086(A)

- 64-4 -Permits
- 62-4.030
- 62-4.040
- 62-4.050
- 62-4.060
- 62-4.070
- 62-4.080
- 62-4.090
- 62-4.100
- 62-4.120
- 62-4.130
- 62-4.160
- 62-4.210
- 62-103-Rules of Administrative Procedure
- 62-204.800(8)-Emissions Guidelines for Municipal Waste Combustors incorporated by reference.
- 62-210 Stationary Sources General Requirements



LIST OF APPLICABLE REGULATIONS

62.	-21	U	20	ነበ

- 62-210.300 -Permits Required
- 62-210.300-Exemptions
- 62-210.300(3)(a)5 –Exemption for internal combustion engines
- 62-210.300(3)(a)16 Exemption for brazing, soldering or welding equipment
- 62-210.300(3)(a)20 & (3)(a)21 -Exemption for emergency electrical generators, heating units, etc.
- 62-210.300(3)(a)22-Fire & Safety Equipment
- 62-210.300(5)-Notification of Startup
- 62-210.350-Public Notice & Comment
- 62-210.360-Admin. Permit Corrections
- 62-210.370(3)-Annual Operating Reports
- 62-210.650-Circumvention
- 62-210.700-Excess Emissions
- 62-210.900-Forms & Instructions
- 62-212.400 Stationary Sources Preconstruction Review, Prevention of Significant Deterioration (PSD)
- 62-212.500-Best Achievable Compliance Technology
- 62-213 Operating Permits for Major Sources
- 62-296- Stationary Sources Emissions Standards
- 62-296.320-General Pollutant Emission Limiting Standards
- 62-296.401(2)
- 62-296.416(3)-Specific Emission Limiting Standard for Mercury
- 62-297.310(2)-Required Number of Tests
- 62-297.310(3)-Calculation of Emission Rates
- 62-297.310(4)-Applicable Test Procedures
- 62-297.310(5)-Determination of Process Variables



LIST OF APPLICABLE REGULATIONS

62-297.310(6)-Required Stack Sampling Facilities

62-297.310(7)-Frequency of Compliance Tests

62-297.310(8)-Test Reports

62-297.620-Exceptions and Approval of Alternate Procedures and Requirements



COMPLIANCE ASSURANCE MONITORING (CAM)
PLAN



COMPLIANCE ASSURANCE MONITORING (CAM) PLAN

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INTRODUCTION

On October 3, 1997 EPA promulgated new rules under 40 CFR Part 64 and revised 40 CFR Parts 70 and 71 to implement Compliance Assurance Monitoring (CAM) for major stationary sources of air pollution that are required to obtain permits under Title V of the Clean Air Act (the "Act"). Subject to certain exemptions, the CAM rule requires owners or operators of such sources to conduct monitoring that satisfies particular criteria provided in the rule to provide a reasonable assurance of compliance with applicable requirements under the Act. The CAM rule applies to all new and renewal Title V applications submitted after April 22, 1998.

The CAM rule is directed at large emission units that rely on control equipment to achieve compliance with the Act. The goal of CAM is to assure that the control devices for these emission units are properly operated and maintained. Monitoring is conducted to ensure that the control devices continue to maintain a level of control that complies with applicable requirements.

APPLICABILITY DETERMINATION

The first step in the CAM process is the determination of the applicability of the CAM rules in 40 CFR Part 64 to each pollutant-specific emissions unit ("unit"). Any unit subject to CAM rules must satisfy all of the criteria included in Section 64.2, which include the following:

- 1. The unit must be located at a major source that is required to obtain a Part 70 or 71 permit
- 2. The unit is subject to an emission limitation or standard for the applicable pollutant
- 3. The unit uses a control device to achieve compliance with the emission limitation or standard
- 4. Potential pre-control emissions of the applicable pollutant from the unit are at least 100% of major source amount
- 5. The unit is not otherwise exempt

Malcolm Pirnie completed a CAM applicability determination for each unit at the City of Tampa's McKay Bay Refuse to Energy Facility (the "Facility"). The rationale for the determination is presented in the sections that follow. Whenever possible, estimates of potential pre-control emissions were calculated using actual stack test data or emission factors obtained from the EPA's Compilation of Air Emission Factors (AP-42). Potential pre-control emission estimates for pollutants not listed in AP-42 were calculated from stack test data and known (or assumed) control device efficiencies. Post-control estimates for pollutant subject to CAM were based on published emission factors, stack test data, or Continuous Emissions Monitoring System (CEMS) data. Emission factors calculated in the EPA's Compilation of Air Emission Factors (AP-42) assumed a waste HHV of 4,500 Btu/lb. and were corrected for the 5,000 Btu/lb assumption used at the Facility. A summary of the determination results is included as Table 1.



Ash Building and Handling System (Emissions Unit No. 100)

Description

The ash building and handling system consists of the ash conveyors, grizzly scalper, and an enclosed prefabricated metal structure at the terminus of the ash collection system that stores the ash prior to landfilling. Fly ash discharged to the collection system from various points in the combustion trains is wetted to prevent fugitive emissions and mixed with bottom ash. The wet combined ash is then conveyed to the grizzly scalper, where large ferrous metals are removed. The wet ash continues on to the ash building, where smaller ferrous and nonferrous metals are removed. The finished ash is discharged to the ground floor and stored for later transport to the Hillsborough County Southeast Landfill. The ash building is equipped with two wet scrubbers to control particulate emissions.

Particulate (PM/PM10)

The existing Title V operation permit limits particulate emissions from the ash building under Florida permit no. PSD-FL-086(A). The ash building is equipped with a baghouse to control particulate emissions. The pre-control emissions factor for the wetted ash was calculated using the predictive emission factor equation in AP-42 Section 13, *Aggregate Handling and Storage Piles*.

AP-42 references landfill fly ash with 27% moisture content as a typical material used in the predictive equation. The wetted ash stored in the ash building is a similar material, with moisture content ranging from 13-22%. In order to provide a conservative estimate, the largest particle size multiplier (0.74), the lowest moisture content (13%), and an estimated wind speed of 5 mph was used in the equation. Calculations for potential pre-control particulate emissions estimates for the wetted ash are shown on the following page. The estimated potential uncontrolled emissions are below the major source threshold for PM, so the CAM rule does not apply to the ash building at the Facility for particulate emissions.

Opacity (VE)

Opacity is regulated under Florida permit no. PSD-FL-086. However, there is no major source threshold defined for opacity in 40 CFR 60. Therefore, the CAM rule does not apply to the ash building and handling system at the Facility for opacity emissions.



Pre-Control PM Estimate

 $E = Emission Factor^{1}$

k = Particle size multiplier (0.74)

U = Mean wind speed (5 mph)

M = Material moisture content (13%)

$$E = k*(0.0032)* (U/5)^{1.3} (M/2)^{1.4}$$

E =
$$0.74*(0.0032)*(5/5)^{1.3} = 1.72$$
 E-04 lb./ton $(13/2)^{1.4}$

Emission factor x ton conversion x design feed rate² x operating time³ = PM emissions estimate $(1.72 \text{ E-04 lb./ton}) \times (\text{ton/2,000 lb.}) \times (\text{60 tons/hr.}) \times (8,760 \text{ hrs./yr.}) = 0.04 \text{ tons/yr.}$

0.04 tons/yr. < 100 tons/yr. (major source threshold for PM), so CAM rules are not applicable to PM for the ash building.

- ¹ Emission factor from AP-42, Vol. 1, Chapter 13, predictive emission factor equation 1)
- ² Design feed rate for the ash building is 60 tons per hour.
- ³ Operating time is based on 100% availability. Actual operating time is less than 8,760 hours per year.

Lime Silos (Emissions Unit No. 101)

Description

The Facility is equipped with two lime storage silos that store pebble lime used in the production of lime slurry for the dry scrubbers. The silos are equipped with a common fabric vent filter to remove entrained lime from conveying air vented during loading operations.

Particulate (PM/PM10)

Turbulent conditions in the lime silos during loading operations entrain lime particles in the conveying air. As the air moves through the silos, the heavier particles settle out in areas of low air velocity. The remaining particles are removed by the vent filters in the baghouse above the silos. The turbulent conditions that generate particulate emissions only exist in the lime silos when conveying air (and new lime) enters the silos during loading operations. Lime loading operations are only performed at the Facility approximately 6 hours per week, but will be conservatively estimated at 500 hours per year.

The existing Title V operation permit limits particulate emissions from the lime silos under permit no. PSD-FL-086. The silos use a control device (baghouse) to achieve compliance with the particulate emission limitation. Potential pre-control particulate emissions estimates are calculated below.



Pre-Control PM Estimate

Emission Factor¹ x ton conversion x design fill rate² x operating time³ = PM emissions estimate $(0.61 \text{ lb./ton}) \times (\text{ton/2,000 lb.}) \times (20 \text{ tons/hr.}) \times (500 \text{ hrs./yr.}) = 3.1 \text{ tons/yr.}$

3.1 tons/yr. < 100 tons/yr. (major source threshold for PM), so CAM rules are not applicable to PM for the lime silo unit.

- ¹ Uncontrolled Particulate Matter Emission Factor for Lime Product Processing and Handling (from AP-42, Vol. 1, Chapter 11), factor for product loading, enclosed truck.
- ² Lime silo design fill rate used as a conservative estimate. Actual fill rate may be less.
- ³ Operating time is based on 500 hours per year. Actual operating time may be less.

Opacity (VE)

Opacity is regulated under Florida permit no. PSD-FL-086. However, there is no major source threshold defined for opacity in 40 CFR 60. Therefore, the CAM rule does not apply to the lime silo at the Facility for opacity emissions.

Activated Carbon Silos (Emissions Unit No. 102)

Description

The Facility is equipped with two activated carbon storage silos that store activated carbon used for mercury control in the MWC units. Each silo is equipped with a fabric vent filter to remove entrained carbon from conveying air vented during loading operations.

Particulate (PM/PM10)

Turbulent conditions in the carbon silos during loading operations entrain carbon particles in the conveying air. As the air moves through the silos, the heavier particles settle out in areas of low air velocity. The remaining particles are removed by the vent filters in the baghouse above the silos. The turbulent conditions that generate particulate emissions only exist in the carbon silos when conveying air (and new carbon) enters the silos during loading operations. Carbon loading operations are only performed at the Facility approximately 3 hours per month, but will be conservatively estimated at 100 hours per year.

The existing Title V operation permit limits particulate emissions from the carbon silos under permit no. PSD-FL-086. The silos use a control device (baghouse) to achieve compliance with the particulate emission limitation. Potential pre-control particulate emissions estimates are calculated below.



Pre-Control PM Estimate

Emission Factor¹ x ton conversion x design fill rate² x operating time³ = PM emissions estimate $(0.58 \text{ lb./ton}) \times (\text{ton/2,000 lb.}) \times (20 \text{ tons/hr.}) \times (100 \text{ hrs./yr.}) = 0.58 \text{ tons/yr.}$

0.58 tons/yr. < 100 tons/yr. (major source threshold for PM), so CAM rules are not applicable to PM for the carbon silo unit.

- ¹ Uncontrolled Particulate Matter Emission Factor for Carbon Black Manufacture (from AP-42, Vol. 1, Chapter 6), factor for pneumatic system vent, bag filter.
- ² Carbon silo design fill rate used as a conservative estimate. Actual fill rate may be less.
- ³ Operating time is based on 100 hours per year. Actual operating time may be less.

Opacity (VE)

Opacity is regulated under Florida permit no. PSD-FL-086. However, there is no major source threshold defined for opacity in 40 CFR 60. Therefore, the CAM rule does not apply to the carbon silo at the Facility for opacity emissions.

Municipal Waste Combustor Units (Emissions Unit Nos. 103, 104, 105, and 106)

Description

The Facility is equipped with four stationary mass-burn waterwall municipal waste combustor (MWC) units, each rated for a maximum heat input capacity of 120 MMBtu/hr. The heat input capacity is comparable to a feed rate of approximately 288 tons per day at 5,000 Btu/lb. Emissions are controlled on each combustion train by a spray dryer absorber, fabric filter baghouse, powdered activated carbon injection and selective non-catalytic reduction (SNCR) systems. Using lime slurry, the scrubber neutralizes acid-forming gases such as hydrogen fluoride, sulfur dioxide, and hydrogen chloride. Activated carbon is injected into the economizer outlet duct to control mercury emissions. The baghouse captures particulate matter entrained in the flue gas. Captured dry ash particles fall into hoppers where they are discharged to the ash collection system.

All four MWC units are permitted major sources under the existing Title V operations permit No. 0570127-004-AV. The pollutants regulated under that permit and their CAM applicability are shown in Table 1.



Table 1 – CAM Applicability Review Summary

			CAN	M Applicabili	ł.v.						CAM Plan Requirements
							_				CAM Fian Requirements
Parameter	40 CFR 60 Subpart Cb NSPS Emission Limit	PSD-FL-086 Emission Limit	Test (1) The unit is subject to an emission limitation or standard for the applicable regulated air pollutant (or a surrogate thereof), other than an emission limitation or standard that is exempt under paragraph (b)(1)	control device to achieve compliance with any such emission limitation or standard	Test (3) The unit has potential pre-control device emissions of the applicable regulated air pollutant that are equal to or greater than 100 percent of the amount, in tons per year, required for a source to be classified as a major source.	CAM applicable? If Tests (1), (2), and (3) are all yes, then CAM applies.	by CEMS	Comments	Monitoring Parameters	Design Pollutant Averaging Period	The unit has the potential to emit, including the effect of control devices, the applicable regulated air pollutant in an amount equal to or greater than 100 percent of the amount, in tons per year, required for a source to be classified as a major source. If yes, data collection requirements of 40 CFR 64 paragraph b(4)(ii) apply.
Ash Building and	d Handling System (Em	issions Unit 100)									
Opacity (VE)		5%	Yes - Regulated under PSD-FL-086	Yes - Wet Scrubbers	No - Major source threshold not defined	No		No major source threshold for opacity			
Lime Storage Sil	os (Emissions Unit 101)									
Particulate (PM/PM10)		0.015 gr/dscf, up to 0.36 lb/hr.	Yes - Regulated under PSD-FL-086	Yes - Baghouse	No - PTE < 100 tpy	No		Pre-control PTE based on uncontrolled emission factor from AP-42, Volume 1, Chapter 11			
Opacity (VE)		5%	Yes - Regulated under PSD-FL-086	Yes - Baghouse	No - Major source threshold not defined	No		No major source threshold for opacity			
Activated Carbo	n Storage Silos (Emissi	ous Unit 102)						Pre-control PTE based on			
Particulate (PM/PM10)		0.015 gr/dscf, up to 0.36 lb/hr.	Yes - Regulated under PSD-FL-086	Yes - Baghouse	No - PTE < 100 tpy	No		uncontrolled emission factor from AP-42, Volume 1, Chapter 6			
Opacity (VE)		5%	Yes - Regulated under PSD-FL-086	Yes - Baghouse	threshold not defined	No		No major source threshold for opacity			
Municipal Waste	e Combustor Units 1-4	(Emissions Units 103, 104									
Particulate (PM/PM10)	27mg/dscm	27 mg/dscm, 0.0230 lb/MMBtu, 2.76 lbs./hr, 12.1 tons/yr per unit.	Cb	Yes - Baghouse	Yes - PTE >100 tpy	No		Regulated under Subpart Cb - Exempt			
Opacity (VE)	10%	10%	No - Regulated under Subpart Cb	Yes - Baghouse	threshold not defined	No	х	Regulated under Subpart Cb - Exempt			
Cadmium (Cd)	0.040 mg/dscm	3.42E-05 lb/MMBtu, 4.10E-03 lbs./hr, 0.0179 tons/yr	Yes - Regulated under Subpart Cb and PSD-FL-086	Yes - Baghouse	No - PTÉ <10 tpy	No		Pre-control PTE based on uncontrolled emission factor from AP-42, Volume 1, Chapter 2			
Lead (Pb)	0.44 mg/dscm	0.44 mg/dscm, 3.76E-04 lb/MMBtu, 0.0451 lbs./hr, 0.197 tons/yr	No - The PSD implements Subpart Cb	Yes - Baghouse	Yes - PTE >5 tpy	No		Regulated under Subpart Cb - Exempt			
Mercury (Hg)	0.080mg/dscm or 15% of potential mercury emission concentration, whichever is less stringent	0.070 mg/dscm, 0.0605 ton/yr.	Yes - Regulated under Subpart Ch and PSD-FL-086	Yes - Carbon System	No - PTE <10 tpy	No		Pre-control PTE based on uncontrolled emission factor from AP-42, Volume 1, Chapter 2			
Sulfur Dioxide (SO2)	29 ppm or 25% of the potential SO2 emission concentration, whichever is less stringent	29 ppm or 25% of the potential SO2 emission concentration, whichever is less stringent. Facility-wide emissions shall not exceed 460 tons in any consecutive 12-month period.	No - The PSD implements Subpart Cb	Yes - Scrubber	Yes - PTE >100 tpy	No	x	Regulated under Subpart Cb - Exempt			
Hydrogen Chloride (HCl)	29 ppm or 5% of the potential HCl emission concentration, whichever is less stringent	29 ppm or 5% of the polential HCl emission concentration, whichever is less stringent, and 67.9 tons/yr.	No - The PSD implements Subpart Cb	Yes - Scrubber	Yes - PTE > 10 tpy	No		Regulated under Subpart Cb - Exempt			
Dioxins/Furan s	For non-electrostatic precipitator controls, 30 ng/dscm	30 ng/dscm, 2.56x10-8 lbs/MMBtu, 3.07x10-6 lbs/hr and 1.35xE-05 tons/year.	Yes - Regulated under Subpart Cb and PSD-FL-086	Yes - Carbon System	No - PTE <10 tpy	No		Pre-control PTE based on uncontrolled emission factor from AP-42, Volume 1, Chapter 2			
Nitrogen Oxides (NOx)	205 թթուս	205 ppmdv, 0.0995 lbs/MMBtu, 11.9 lbs/fr. Facility-wide emissions shall not exceed 679 tons in any consecutive 12-month period.	No - The PSD implements Subpart Cb	Yes - Thermal Denox (Urea)	Yes - PTE > 100 tpy	No	x	Regulated under Subpart Cb - Exempt			
Carbon Monoxide (CO)		100 ppmdv on 4 hr block avg, 0.0995 lb/MMBtu, 11.9 lbs/hr. Facility-wide emissions shall not exceed 185 tons in any consecutive 12-month period.	Yes - Regulated under Subpart Cb and PSD-FL-086	No	Yes - PTE > 100 tpy	Νο	х	No control device			
Fluoride (F)		0.0125 lb/MMBtu, 1.5 lbs/hr and 6.57 tons/year per unit.	Yes - Regulated under PSD-FL-086	Yes - Scrubber	No - PTE <10 tpy	No		PTE based on 2001 stack test data and assumed 90% control efficiency			
Beryllium (Be)		9.58E-07 lb/MMBtu, 0.000115 lb/hr and 5.04E-04 tons/yr per unit.	Yes - Regulated under PSD-FL-086	Yes - Baghonse	No - PTE <10 tpy	No		PTE based on 2001 stack test data and assumed 99.9% control efficiency			



Particulate (PM/PM10)

Particulate matter generated during solid waste combustion is comprised of both unburned combustible material and inert material that was present in the solid waste. Turbulent conditions in the combustor entrain this material in the flue gas as fly ash. As the flue gas moves through the boiler and heat recovery equipment, the heavier particles settle out in areas of low gas velocity (i.e. hoppers and scrubbers) and are removed. The remaining particles are removed by the fabric filters in the baghouses.

PSD-FL-086(A) limits PM emissions from the MWC units to 27 mg/dscm, corrected to 7% O₂. The PSD permit implements the federal 40 CFR 60, Subpart Cb requirements, so Subpart Cb governs the regulation of PM at the facility. Therefore, the facility is exempt from CAM requirements for particulate matter. The additional PSD limits for PM (0.0230 lb/MMBtu, 2.76 lb/hr, and 12.1 ton/yr) are equivalents of the Federal limit, as shown in the following calculations:

PM Equivalency Calculations

PM limit in 40 CFR 60.33b = 27 mg/dscm, corrected to $7\% O_2$

MWC Flowrate = 27,289.8 dscfm (original retrofit flowrate assumption), corrected to $7\% O_2$

(27 mg/dscm) / (2288.4) = 0.0118 gr/dscf

 $(0.0118 \text{ gr/dscf}) \times (27,289.8 \text{ dscf/min}) \times (g/15.43 \text{ gr}) \times (60 \text{ sec/min}) = 0.348 \text{ g/s}$

 $(0.348 \text{ g/s}) \times (3600 \text{ s/hr}) \times (0.0022) \text{ lb/g} = 2.76 \text{ lb/hr}$

 $(2.76 \text{ lb/hr}) \times (8760 \text{ hr/yr}) / (2000 \text{ lb/ton}) = 12.1 \text{ tons/yr}$

2.76 lb/hr / 120 MMBtu/hr = 0.0230 lb/MMBtu

PM limits in PSD-FL-086 = 0.0230 lb/MMBtu, 2.76 lb/hr, 12.1 ton/yr

Opacity (VE)

Opacity is regulated under 40 CFR 60, Subpart Cb and is therefore exempt from the CAM rule.

Cadmium (Cd)

Cadmium is a trace metal found in many components of solid waste, and is volatilized during combustion. Cadmium will solidify in the cooler areas of the heat recovery equipment by condensing on the surface of entrained particles in the flue gas or will form particulate itself. These particles are carried in the flue gas stream to the baghouse, where they settle out by gravity or are captured on the



filter bag surface and removed. Therefore, the capture of particulate matter in the baghouse results in the capture of cadmium.

The existing Title V operation permit limits cadmium emissions from the MWC units under permit no. PSD-FL-086(A). The MWC units use a control device (baghouse) to achieve compliance with the lead emission limitation. However, the pre-control cadmium emission estimate is below the major source threshold, so the CAM rule does not apply to the MWC units at the Facility for cadmium emissions. Potential pre-control cadmium emissions are calculated below.

Pre-Control Cd Estimate

Emission factor¹ Btu conversion $(1.09 \text{ E-}02 \text{ lb./ton}) \times (5,000/4,500) = (1.21 \text{ E-}02 \text{ lb./ton})$

Emission Factor x ton conversion x design feed rate² x operating time³ = Cd emissions estimate $(1.21 \text{ E-}02 \text{ lb./ton}) \times (\text{ton/}2,000 \text{ lb.}) \times (12 \text{ tons/hr.}) \times (8,760 \text{ hrs./yr.}) = 0.64 \text{ tons/yr.}$

0.64 tons/yr. < 10 tons/yr. (major source threshold for Cd), so CAM rules are not applicable to Cd for all MWC units.

- ¹ Uncontrolled Cadmium Emission Factor for Mass Burn Combustors (from AP-42, Vol. 1, Chapter 2) used a heating value of 4,500 Btu/lb. The Facility reference waste heating value is 5,000 Btu/lb.
- ² MWC maximum feed rate used as a conservative estimate. Actual feed rate may be less.
- ³ Operating time is based on 100% availability. Actual operating time is less than 8,760 hours per year.

Lead (Pb)

Lead is a trace metal found in most components of solid waste, and is readily volatilized during combustion. Lead vapor will solidify in the cooler areas of the heat recovery equipment by condensing on the surface of entrained particles in the flue gas or will form particulate itself. These particles are carried in the flue gas stream to the baghouse, where they settle out by gravity or are captured on the filter bag surface and removed. Therefore, the capture of particulate matter in the baghouse results in the capture of lead. A fraction of the lead remains as fine particulate and will escape capture in the control device.

PSD-FL-086(A) limits Pb emissions from the MWC units to 0.44 mg/dscm, corrected to 7% O₂. The PSD permit implements the federal 40 CFR 60, Subpart Cb lead requirement, so Subpart Cb governs the regulation of Pb at the facility. Therefore, the facility is exempt from CAM requirements for lead. The additional PSD limits for lead (3.76E-04 lb/MMBtu, 0.0451 lb/hr, and 0.197 ton/yr) are equivalents of the Federal limit, as shown in the following calculations:



Pb Equivalency Calculations

Pb limit in 40 CFR 60.33b = 0.44 mg/dscm, corrected to $7\% O_2$

MWC Flowrate = 27,289.8 dscfm (original retrofit flowrate assumption), corrected to $7\% O_2$

 $(27,289.8 \text{ dscfm}) / (35.31 \text{ dscf}) \times (60 \text{ sec}) = 12.881 \text{ dscm/sec}$

 $(44\mu g/dscm) \times (12.881 dscm/sec) / (106 \mu g) = 0.00567 g/sec$

 $(0.00567 \text{ g/sec}) \times (3600 \text{ sec/hr}) \times (0.0022 \text{ lb/g}) = 0.045 \text{ lb/hr}$

 $(0.045 \text{ lb/hr}) \times (8,760 \text{ hr/yr}) / (2000 \text{ lb/ton}) = 0.197 \text{ ton/yr}$

(0.045 lb/hr) / (120 MMBtu/hr) = 3.75 E - 04 lb/MMBtu

Pb limits in PSD-FL-086(A) = 0.000376 lb/MMBtu, 0.0451 lb/hr, 0.197 ton/yr

Mercury (Hg)

Mercury is also a trace metal found in solid waste that is readily volatilized during combustion. Mercury vapor condenses on the surface of entrained particles in the flue gas, especially fine particulates because of the high surface area to volume ratio. Activated carbon is injected into the scrubber to provide a fine particulate surface on which the mercury vapor can adsorb or condense, which effectively removes mercury from the flue gas. The mercury-laden particles are then carried in the flue gas stream to the baghouse, where they settle out by gravity or are captured on the filter bag surface and removed. Therefore, the capture of particulate matter in the baghouse results in the capture of mercury. A very small fraction of the mercury remains as fine particulate and will escape capture in the control device.

Florida permit no. PSD-FL-086(A) limits mercury emissions from the MWC units. The MWC units use control devices (scrubber and baghouse) to achieve compliance with the lead emission limitation. However, the pre-control mercury emission estimate is below the major source threshold, so the CAM rule does not apply to the MWC units at the Facility for mercury emissions. The potential pre-control mercury emissions estimate calculation is shown below.



Pre-Control Hg Estimate

Emission factor¹ Btu conversion $(5.60 \text{ E}-03 \text{ lb./ton}) \times (5,000/4,500) = (6.22 \text{ E}-03 \text{ lb./ton})$

Emission Factor x ton conversion x design feed rate² x operating time³ = Hg emissions estimate $(6.22 \text{ E-}03 \text{ lb./ton}) \times (\text{ton/}2,000 \text{ lb.}) \times (12 \text{ tons/hr.}) \times (8,760 \text{ hrs./yr.}) = 0.33 \text{ ton/yr.}$

0.33 ton/yr. < 10 tons/yr. (major source threshold for Hg), so CAM rules are not applicable to Hg for both MWC units.

- ¹ Uncontrolled Mercury Emission Factor for Mass Burn Combustors (from AP-42, Vol. 1, Chapter 2) used a heating value of 4,500 Btu/lb. The Facility reference waste heating value is 5,000 Btu/lb.
- ² MWC design feed rate used as a conservative estimate. Actual feed rate may be less.
- ³ Operating time is based on 100% availability. Actual operating time is less than 8,760 hours per year.

Sulfur Dioxide (SO₂)

Sulfur dioxide formation is a function of the chemical form and content of sulfur in the solid waste fuel. Sulfur occurs in organic and inorganic forms and usually converts to SO₂ during combustion. A small amount of SO₂ generated during solid waste combustion is further oxidized to SO₃, which combines with water to form sulfuric acid (H₂SO₄) mist, or SAM. SAM is discussed later as a separate pollutant.

Flue gas containing sulfur dioxide enters the dry scrubbers, where it comes in contact with finely atomized alkaline (lime) slurry. The alkaline slurry chemically reacts with the sulfur dioxide in the flue gas, forming neutralized calcium compounds that settle out in the scrubber hopper or are captured on the baghouse filters.

PSD-FL-086(A) limits SO_2 emissions from the MWC units to 29 ppmdv corrected to 7% O_2 or 75% reduction by weight or volume, whichever is greater. The PSD permit implements the federal Subpart Cb requirements, so Subpart Cb governs the regulation of SO_2 at the facility. Therefore, the facility is exempt from CAM requirements for sulfur dioxide.

Hydrogen Chloride (HCl)

Hydrogen chloride forms during the combustion of solid waste. The amount of HCl formed during combustion depends on the amount of chlorine-containing materials (i.e. salts, PVC, etc.) present in the solid waste.

Flue gas containing hydrogen chloride enters the dry scrubbers, where it comes in contact with finely atomized alkaline (lime) slurry. The alkaline slurry chemically reacts with the HCl in the flue



gas, forming neutralized calcium compounds that settle out in the scrubber hopper or are captured on the baghouse filters.

PSD-FL-086(A) limits HCl emissions from the MWC units to 29 ppmdv corrected to 7% O₂ or 95% reduction by weight or volume, whichever is greater. The PSD permit implements the federal Subpart Cb requirements, so Subpart Cb governs the regulation of HCl at the facility. Therefore, the facility is exempt from CAM requirements for hydrogen chloride.

Dioxins/Furans (PCDD/PCDF)

Dioxins/furans (or MWC organics) are two groups of structurally similar compounds that contain 210 isomers. The chemical, physical, and toxicological characteristics of each isomer vary relative to its chemical structure, but some of the isomers are highly toxic.

Dioxin and furan formation can be minimized by maintaining good combustion practices in combination with scrubbers and fabric filters. The Facility uses scrubbers and fabric filters, but also injects activated carbon into the scrubber, which promotes further removal of dioxins and furans.

The existing Title V operation permit limits dioxin/furan emissions from the MWC units under 40 CFR 60, Subpart Cb and permit no. PSD-FL-086. The MWC units use control devices (scrubber and baghouse) to achieve compliance with the lead emission limitation. However, the pre-control dioxin/furan emissions estimate is below the major source threshold, so the CAM rule does not apply to the MWC units at the Facility for dioxin/furan emissions. The potential pre-control emissions estimate calculation is shown below.

Pre-Control CDD/CDF Estimate

Emission factor¹ Btu conversion $(1.67 \text{ E}-06 \text{ lb./ton}) \times (5,000/4,500) = (1.85 \text{ E}-06 \text{ lb./ton})$

Emission Factor x ton conversion x design feed rate² x operating time³ = CDD/CDF emissions estimate $(1.85 \text{ E-06 lb./ton}) \times (\text{ton/2,000 lb.}) \times (12 \text{ tons/hr.}) \times (8,760 \text{ hrs./yr.}) = 0.00009 \text{ tons/yr.}$

0.00009 tons/yr. < 10 tons/yr. (major source threshold for CDD/CDF), so CAM rules are not applicable to CDD/CDF for all MWC units.

¹ Uncontrolled CDD/CDF Factor for Mass Burn Combustors (from AP-42, Vol. 1, Chapter 2) used a heating value of 4,500 Btu/lb. The Facility reference waste heating value is 5,000 Btu/lb.

² MWC design feed rate used as a conservative estimate. Actual feed rate may be less.

³ Operating time is based on 100% availability. Actual operating time is less than 8,760 hours per year.



Nitrogen Oxides (NO_x)

Nitrogen oxides are products of all conventional combustion processes. NO_x forms during the combustion of solid waste through two mechanisms, thermal NO_x and fuel NO_x . Thermal NO_x is formed by high temperature oxidation of nitrogen in the combustion air, and fuel NO_x is formed by the oxidation of nitrogen in the solid waste. Because of the temperatures at which MWC units operate, 70-80% of NO_x formed is fuel NO_x .

The Facility uses a Selective Non-Catalytic Reduction (SNCR) system to control NO_x concentration in the flue gas. The system injects a mixture of air and urea into the boiler above the stoker grate. The urea reacts with NO_x in the gas path, resulting in the formation of elemental nitrogen, carbon dioxide, and water.

 NO_x emissions from each MWC unit are regulated under 40 CFR 60, Subpart Cb and Florida permit no. PSD-FL-086(A). The PSD includes a Facility-wide NO_x limit of 679 tons per year, which is above the major source threshold of 100 tons/yr for each unit. The City of Tampa intends to use the existing nitrogen oxide CEMS system to demonstrate compliance with the permit limits, thereby exempting NO_x from CAM requirements under 40 CFR 64.2(b)(vi).

Carbon Monoxide (CO)

Carbon Monoxide is formed by the incomplete oxidation of carbon compounds in fuel. Some carbon monoxide is formed during all combustion processes where carbon-containing fuel is used. However, the amount of carbon dioxide formed is dependent upon the combustion efficiency of the fuel –burning process. Incomplete oxidation can be caused by several factors, including:

- Fuel-rich conditions (low oxygen)
- Poor fuel-air mixing
- Low combustion temperature
- Short combustion zone residence time

Carbon monoxide formation can be effectively controlled by designing the combustor to provide an adequate supply of combustion air and maximizing combustion efficiency. The Facility's MWC units control CO through good combustion design and operational practices.

CO emissions from each MWC unit are regulated under 40 CFR 60, Subpart Cb and Florida permit no. PSD-FL-086(A). The Facility does not use a control device to achieve compliance with emission limitations, so the CAM rule does not apply to the MWC units at the Facility for carbon monoxide emissions.

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Fluoride (F)

Fluoride production during solid waste combustion is a function of the fluorine content of the waste (primarily in fluorinated plastics and other fluorocarbons), combustion temperature, and thermally-driven chemical reactions between the combustion air and the fluorine-containing wastes. Fluorides are highly soluble in water and can be effectively controlled by contact with the finely atomized alkaline (lime) slurry in the dry scrubber.

The existing Title V operation permit limits fluoride emissions from the MWC units under Florida permit no. PSD-FL-086(A). The MWC units use a control device (scrubber) to achieve compliance with the fluoride emission limitation. Potential pre-control fluoride emissions estimates are calculated below. No fluoride emission factors were published in AP-42, so the most recent (2004) stack test data for fluoride was used in conjunction with an assumed scrubber control efficiency of 90% to obtain the pre-control emission estimate.

Assuming 90% control efficiency, the pre-control fluoride emission estimate is below the major source threshold. Therefore, the CAM rule does not apply to the MWC units at the Facility for fluoride emissions. The potential pre-control fluoride emissions estimate calculation is shown below.

Pre-Control F Estimate

Emission rate¹ x ton conversion x operating time² x scrubber efficiency factor = F emissions estimate $(0.0027 \text{ lb./hr.}) \times (\text{ton/2,000 lb.}) \times (8,760 \text{ hrs./yr.}) \times (100/100-90) = 0.12 \text{ tons/yr.}$

0.12 tons/yr. < 10 tons/yr. (major source threshold for F), so CAM rules are not applicable to F for the MWC units.

- ¹ Maximum fluoride emissions rate from 2004 stack test
- ² Operating time is based on 100% availability. Actual operating time is less than 8,760 hours per year.

Beryllium (Be)

Beryllium is a metal found only in trace quantities in solid waste, and is much less volatile than lead or mercury. Therefore, most of the beryllium in the solid waste will be retained in the bottom ash after combustion. Small amounts of beryllium vapor will solidify in the cooler areas of the heat recovery equipment by condensing on the surface of entrained particles in the flue gas. These particles are carried in the flue gas stream to the baghouse, where they settle out by gravity or are captured on the filter bag surface and removed. Therefore, the capture of particulate matter in the baghouse results in the capture of beryllium. A small fraction of the beryllium remains as fine particulate and will escape capture in the control device.



Beryllium emissions from each MWC unit are regulated under 40 CFR 60, Subpart Cb and Florida permit no. PSD-FL-086(A). The MWC units use a control device (baghouse) to achieve compliance with the beryllium emission limitation. Potential pre-control beryllium emissions estimates are calculated below. No beryllium emission factors were published in AP-42, so the most recent (2004) stack test data for beryllium was used in conjunction with an assumed scrubber control efficiency of 99.9% to obtain the pre-control emission estimate. Malcolm Pirnie has no data on dry scrubber control efficiencies for beryllium, but an efficiency assumption of 99.9% produces a very conservative estimate of pre-control emissions.

Assuming 99.9% control efficiency, the pre-control beryllium emission estimate is below the major source threshold. Therefore, the CAM rule does not apply to the MWC units at the Facility for beryllium emissions. The potential pre-control beryllium emissions estimate calculation is shown below.

Pre-Control Be Estimate

Emission rate¹ x ton conversion x operating time² x scrubber efficiency factor = Be emissions estimate $(4.2 \text{ E-}05 \text{ lb./hr.}) \times (\text{ton/2,000 lb.}) \times (8,760 \text{ hrs./yr.}) \times (100/100-99.9) = 0.042 \text{ tons/yr.}$

0.042 tons/yr. < 10 tons/yr. (major source threshold for Be), so CAM rules are not applicable to Be for the MWC units.

- ¹ Maximum beryllium emissions rate from 2004 stack test
- ² Operating time is based on 100% availability. Actual operating time is less than 8,760 hours per year.



REQUESTED CHANGES TO TITLE V AIR OPERATIONS PERMIT



REQUESTED CHANGES TO TITLE V OPERATING PERMIT

No changes are requested in this application.



EMISSIONS UNIT ADDITIONAL INFORMATION ADDITIONAL REQUIREMENTS FOR ALL APPLICATIONS



FUEL ANALYSIS OR SPECIFICATIONS



FUEL SPECIFICATION

The primary fuel for the Facility is municipal solid waste (MSW), including the items and materials that fit within the definition of MSW contained in either 40 CFR 60.51b or Section 403.706(5), Florida Statutes. Secondary fuel is natural gas for the auxiliary burners used during boiler startups, shutdowns, and malfunctions.

The following other solid waste may be used as fuel at the Facility:

- a) Confidential, proprietary, or special documents (including but not limited to business records, lottery tickets, event tickets, coupons, and microfilm);
- b) Contraband which is being destroyed at the request of appropriately authorized local, state, or federal government agencies, provided that such material is not an explosive, a propellant, a hazardous waste, or otherwise prohibited a the facility. Contraband includes but is not limited to drugs, narcotics, fruits, vegetables, plants, counterfeit money, and counterfeit consumer goods;
- c) Wood pallets, clean wood, and land clearing debris;
- d) Packaging materials and containers;
- e) Clothing, natural and synthetic fibers, fabric remnants, and similar debris, including but not limited to aprons and gloves; or
- f) Rugs, carpets and floor coverings, but not asbestos-containing materials or polyethylene or polyurethane vinyl floor coverings

Waste tires may be used as fuel at the facility. However, waste tires received as segregated loads shall not exceed 3%, by weight, of the facility's total fuel. Compliance with this limitation shall be determined by using a rolling 30-day average in accordance with specific condition A.81 of PSD-FL-086(A).

The following non-MSW material may also be used as fuel at the facility. The total quantity of non-MSW material received as segregated loads shall not exceed 5%, by weight, of the facility's total fuel. Compliance with this limitation shall be determined by using a rolling 30-day average in accordance with specific condition A.81 of PSD-FL-086(A).

- a) Construction and demolition debris;
- b) Oil spill debris from aquatic, coastal, estuarine or river environments. Such items or materials include but are not limited to rags, wipes, and absorbents.
- c) Items suitable for human, plant, or domesticated animal use, consumption, or application where the item's shelf life has expired or the generator wishes to remove the items from the



FUEL SPECIFICATION

market. Such items or materials include, but are not limited to off-specification or expired consumer products, pharmaceuticals, medications, health and personal care products, cosmetics, foodstuffs, nutritional supplements, returned goods, and controlled substances.

- d) Consumer-packaged products intended for human or domesticated animal use or application but not consumption. Such items or materials include but are not limited to carpet cleaners, household or bathroom cleaners, polishes, waxes, and detergents.
- e) Waste materials that:
 - 1) Are generated in the manufacture of items in categories (c) or (d) above, and are functionally or commercially useless (expired, rejected or spent); or
 - Are not yet formed or packaged for commercial distribution. Such items or materials must be substantially similar to other items or materials routinely found in MSW.
- f) Waste materials that contain oil from:
 - 1) The routine cleanup of industrial or commercial establishments and machinery; or
 - 2) Spills of virgin or used petroleum products. Such items or materials include but are not limited to rags, wipes, and absorbents.
- g) Used oil and used oil filters. Used oil containing a PCB concentration equal to or greater than 50 ppm shall not be burned, pursuant to the limitations of 40 CFR 761.20(e).
- h) Waste materials generated by manufacturing, industrial or agricultural activities, provided that these items or materials are substantially similar to items or materials that are routinely found in MSW, subject to prior approval of the Department.

Auxiliary burners for each MWC unit shall be fired only with natural gas. The annual capacity factor for natural gas for each unit shall be limited to 10% or less in accordance with PSD-FL-086(A).

DETAILED DESCRIPTION OF CONTROL EQUIPMENT

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City of Tampa McKay Bay Refuse to Energy Facility Retrofit Project Operation & Maintenance Manual

II. GENERAL DESCRIPTION

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City of Tampa McKay Bay Refuse to Energy Facility Retrofit Project Operation & Maintenance Manual

II. GENERAL DESCRIPTION

Wheelabrator Air Pollution Control has supplied the following major components for the City of Tampa McKay Bay Refuse to Energy Facility Retrofit Project.

- A Spray Dryer Absorber/Fabric Filter (SDA/FF) Dry Scrubbing System with Absorbent Preparation System and Powdered Activated Carbon (PAC) Injection, to control acid gas, solid particulates, heavy metal and dioxin/furan emissions from the four refuse fired boilers.
- A Selective Non Catalytic Reduction (SNCR) System to control Nitrogen Oxide (NO₂) formation in the boiler.
- A Continuous Emissions Monitoring (CEM) to monitor the performance of the two above systems and provide the required compliance data.

1.0 SUMMARY

1.1 Dry Scrubbing System

The Dry Scrubbing System has been designed to provide acid gas (SO₂, HCl), solid particulate (dust), heavy metal and dioxin/furan control from each of four (4) refuse fired boilers. The Dry Scrubbing System consists of a Spray Dryer Absorber (SDA) and a Fabric Filter (FF) for each boiler.

Flue gas enters the top of each SDA. Lime slurry is atomized into the flue gas in the SDA. The fine spray droplets absorb acid gases (SO2, HCl) from the flue gas. The heat of the flue gas evaporates the slurry water creating a solid particle. The flue gas is then ducted to a fabric filter where the fly ash from the boiler and the dried reaction products from the SDA are collected. Additional acid gas removal occurs as the flue gas passes through the dust on the fabric filter bags. Two lime slurry preparation systems are provided to prepare the lime slurry. Redundant slakers are provided to mix the pebble lime with city water and make the lime slurry (Ca(OH)_b). The slurry is stored in redundant lime slurry storage tanks and pumped through a complete recirculation loop to the four SDA's. Wastewater from the plant is piped to a dilution water tank and pre-softened with some of the lime slurry. This water is also pumped to the SDA'S. The



evaporation of the slurry water in the SDA cools the flue gas. This causes heavy metals and dioxin/furans that exist as vapors at the SDA inlet to condense.

To further enhance the collection of mercury and dioxin/furans, powdered activated carbon (PAC) will be injected upstream of each SDA. The PAC adsorbs additional mercury and dioxin/furans. Two PAC injection systems are provided, one for each pair of boilers. PAC is stored in a silo and is fed to three (2 operating /1 spare) feeder/educator assemblies for each pair of boilers. The educator pneumatically conveys the PAC to the SDA inlet ductwork where is it injected it into the boiler flue gas.

1.2 SNCR NOx Control System

The SNCR NO_x Control System injects a urea-based solution (NO_xOUT A) into the boiler to reduce nitrogen oxide emissions to nitrogen and water. NO_xOUT A is a mixture of urea and proprietary chemicals. It is stored in a common storage tank. A circulation module pumps the solution to four metering modules, one per boiler. The metering individual modules mix a controlled amount of concentrated solution with dilution water. The diluted reagent is then pumped to four distribution modules. The reagent is then transported to eight injector nozzles per boiler where compressed air is added to atomize the solution. The air / reagent mixture is injected into the boiler off gas above the boiler overfire air ports. The dilute urea decomposes and then reacts with the NO_x to form harmless nitrogen gas.

1.3 Continuous Emission Monitoring System

A Continuous Emission Monitoring System is utilized to measure, record and report the performance of the individual boiler trains and their emission control systems to the local Environmental Authorities. Table 1.3 summarizes the data that will be collected. A dedicated multi-component analyzer will be supplied for the inlet of each SDA and the outlet of each FF. An in situ opacity monitor will be installed at each fabric filter outlet. The analyzers are a "Hot-Wet" extractive design. A representative flue gas sample is extracted, filtered and conveyed by heated sampling lines to the analyzer. The analyzer will also be heated to prevent condensation of the moisture in the sample. The outlet test stations are also equipped with opacity monitors. The analyzers are located in an enclosure along with the Data Acquisition System. Sulfur Dioxide (SO₂) and Nitrogen Oxides (NO_x) signals are fed back via the DCS to the Dry Scrubbing and SNCR Systems. These signals will be used to adjust lime slurry flow (Dry Scrubbing) and NOxOut Solution (SNCR) feed to maintain compliance.



The CEM System is supplied by Aldora. Please refer to their manual for additional information and operating instructions.

Table 1.3 CEM Measurement Da	ata	
SDA Inlet		
CO ₂ SO ₂ CO (Low) CO (High) H ₂ O O ₂	0-20% 0-600 0-100 0-2,000 0-25% 0-25%	Dgb ppm-dgb ppm-dgb ppm-dgb wgb
FF Outlet CO ₂ SO ₂ NO _x H ₂ O O ₂ Opacity	0-20% 0-150 0-400 0-25% 0-25% 0-100%	dgb ppm-dgb ppm-dgb wgb wgb
Recorded Process Parameters	SDA Outlet Temperature PAC Feeder Speed Boiler Stream Flow	



2.0 DRY SCRUBBING SYSTEM

The Dry Scrubbing System is designed to provide HCl, SO, and acid gas, solid particulate, heavy metal and dioxin/furan control. Calcium hydroxide slurry (Ca(OH),) is atomized into the flue gas using a Spray Dryer Absorber (SDA). See process flow diagrams, drawings 04-21-3-001 and 002. Acid gases are absorbed by the slurry, while the heat of the flue gas evaporates the slurry water, and cools the flue gas. The cooled gas is directed to a fabric filter where solid particulates (fly ash and dried reaction products) are collected. Cooling the flue gas promotes the condensation of heavy metals (mercury, cadmium, lead) and dioxin/furans, allowing them to be captured as a solid or aerosol in the fabric filter. Powdered Activated Carbon (PAC) is pneumatically injected upstream of the SDAs. The PAC adsorbs mercury and dioxin/furans from the flue gas.

Design Removal/Emission levels are:

SO₂ Least stringent of 29 ppm_{v-dsb} @ 7% O₂ (24 hr geometric mean) outlet

concentration

- or -

80% removal (24 hr geometric mean)

HC1 Least stringent of 25 ppm_{v-dgb} @ 7% O₂ outlet concentration

- or -

95% removal

Solid Particulate Outlet concentration less than 0.010 gr/dscf @ 7% O₂ (24 mg/dscm)

Opacity (%) Less than 10% (6 min avg.)

PCDD/PCDF Outlet concentration less than 13 ng/DSCM @ 7% O₂ total

PCDD/PCDF

Mercury Least stringent of 85% removal or an outlet concentration less than 70

μg/DSCM @ 7% O₂

Outlet concentration less than 0.20 mg/DSCM @ 7% O₂ Lead

Cadmium Outlet concentration less than 0.020 mg/DSCM @ 7% O₂



2.1 Process Description

2.1.1 Acid Gas Control

Flue gas is ducted from each boiler's economizer to the top of a dedicated spray dryer absorber. An atomized calcium hydroxide (Ca(OH)₂) slurry is used to absorb SO₂ and HCl from the flue gas (see Drawings No. 04-21-3-001 and 002). The slurry and a controlled amount of dilution water are mixed and then atomized with compressed air and injected into the flue gas. The SO₂ and HCl are absorbed by the atomized slurry droplets. The SO₂ reacts with the Ca(OH)₂ to form calcium sulfite (CaSO₃•½H₂O). Some of the calcium sulfite is further oxidized to calcium sulfate (CaSO₄•H₂O) by oxygen in the boiler off gas. The HCl reacts with the Ca(OH)₂ to form CaCl₂. Trace amounts of HF produced by the boiler are also absorbed and solid CaF₂ is produced.

Evaporation of the slurry water in the droplets occurs simultaneously with these reactions. The absorption of SO₂ and HCl continues after the droplet has dried and a solid particle is formed. The flue gas and solid particulate are then directed to a fabric filter where the solid materials are collected from the flue gas. The efficiency of the process is improved as the spray dryer absorber exit temperature decreases and approaches the saturation temperature. A lower exit temperature increases the time required to dry the slurry droplet, thereby increasing the reaction time of the more efficient liquid absorption step. The amount of lime slurry and dilution water that is introduced to the process is controlled to obtain maximum SO₂ and HCl removal, while producing a dry product. The system will be designed to operate, at an outlet temperature setpoint between 275° and 315°F at design conditions. The initial recommended set point is 285°F. The spray dryer absorber is designed to provide eleven (11) seconds residence time, based on the design boiler load of 100 MM BTU/hr and 485°F SDA inlet temperature.

The selected outlet temperature is also critical for the collection of dioxin/furans and heavy metals. WAPC's experience indicates that a maximum outlet temperature of 350°F is required to optimize collection of all the specified heavy metals. CaCl₂ is deliquescent, or in English it means that it will absorb water. Operation at too low of a SDA outlet temperature will cause the dust to clump and become sticky, creating ash handling problems. Once the CaCl₂ has absorbed more water, the dust also become more corrosive.

Additional SO₂ and HCl removal occurs in the fabric filter as the flue gas passes through the filter cake layer on the filter's bags. The fabric filter cleaning sequence is designed to maintain maximum filter cake on the bags to improve acid gas removal in the fabric filter and minimize lime consumption. The cleaning cycle will also be designed to operate based on pressure drop initiated cleaning, with a maximum time interval override. The pressure drop initiation maximizes the time dust is retained on the fabric, for acid gas capture, compared with a straight time interval. The timer override minimizes the upsets that can occur with a rapid increase in boiler load. Cleaning frequency, if based on pressure drop, decreases at lower boiler loads, increasing the thickness of the built up filter cake. If there is a step



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change increase in load, there will be a corresponding large increase in pressure drop. This can require the rapid cleaning of several compartments to maintain the pressure drop setpoint, thereby exposing several compartments of cloth with little or no filter cake to the flue gas.

2.1.2 Heavy Metal and Dioxin/Furan Control

There are specific heavy metal emission limits for mercury (Hg), cadmium (Cd) and lead (Pb). The primary mechanism for heavy metal and dioxin/furan is condensation in the SDA and collection of the subsequent aerosol in the fabric filter. Collection is primarily dependent on fine (sub-micron) particulate collection, and to a lesser degree, SDA outlet temperature. Dioxin/Furan control temperature dependence is insignificant once threshold temperatures are reached. Dioxin/furan and mercury capture improves little as the SDA exit temperature is decreased from 350° to 230°F.

Mercury emissions are present as elemental mercury and mercuric chloride. The elemental mercury is present as a vapor and very little is condensed and collected at the proposed SDA outlet temperatures. Elemental mercury and mercuric chloride collection is improved with the introduction of Powdered Activated Carbon (PAC) into the flue gas upstream of the SDA. Mercury and Mercuric Chloride are adsorbed into the pore structure of the activated carbon. The PAC also improves Dioxin/Furan capture.

PAC is metered into a venturi type educator that pneumatically conveys the material to the ductwork upstream of the flue gas SDA where it is injected into the flue gas. The separate injection system provides a steady flow of PAC, independent of the SDA operation.

For each of the two boilers, there are two PAC silos. There are 3 blowers for each set of two boilers (2 operating/1 spare).

2.1.3 Design Basis

Table 2.1.1 lists the range design conditions at the inlet of the Spray Dryer Absorber (SDA). The SDA has been designed for a maximum slurry water feed rate of 15 gpm. This corresponds approximately to boiler operation at 100 MM BTU/hr at 100% excess air and SDA inlet/outlet temperatures of 485/285 °F.

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Tables 2.1.2 thru 2.1.4 show flow rates and temperatures, at steady state operation for the following conditions.

TABLE	BOILER LOAD	SO,/HCI CONCENTRATION	INLET TEMPERATURE
2.1.2	100% MCR	90% UC1	485
2.1.3	75% MCR	90% UC1	465
2.1.4	110% MCR	Average	495

Tables 2.1.2 thru 2.1.4 show flow rates and temperatures, at steady state operation for the following conditions.

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Table 2.1.1 SDA Inlet Design Parameter (per Boiler)						
oiler Load lue Gas Flow Rate emperature @ Full Load (1)	100 MM BTU/HR					
Flue Gas Flow Rate	146,670 lb/hr 36,701 SCFM 63,487 ACFM					
Temperature @ Full Load (1) Minimum Temperature	495°F 485°F					

Maximum Acid Gas and Particulate at Inlet

	99% UCL ⁽²⁾ Max. Removal Design	90% UCl Lime System Design	Mean
SO ₂ lb/hr	122	77	100
ppm(v-dgb)@7%O ₂	526	77	302
HCl lb/hr	197	143	170
ppm(v-dgb)@7%O ₂	1482	981	1232
HF lb/hr	2	3	3
ppm(v-dgb)@7%O ₂	34	34	34
Solid Particulate 1b/hr	528	576	552
gr/sdcf@7%O ₂	2.6	2.6	2.6

- Return to Figure 2.1.1 to determine maximum temperature at reduced load operation. (1)
- UCL Upper Confidence Limit; eg. 90% UCL: Concentration/flow will be below limit (2) 90% of time.



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APC RETROFIT PROJECT

Absorbent Preperation System Mass Balance

MARCH 26, 1999

Bollet # 1, Case # 8, 100% MCK, 80%EA, Diny Bollet, 90% UCL Boiler # 2; Case # 8; 100% MCR; 80%EA; Dirty Boiler; 90% UCL

Boiler # 3; Case # 8; 100% MCR; 80%EA; Dirty Boiler; 90% UCL Boiler # 4; Case # 8; 100% MCR; 80%EA; Dirty Boiler; 90% UCL

			ستنساخ بالسسام					1.8	L9						
	Slaker	Slaker	Lime	Lime	Lime to Dif	Lime Pump	LIZO to Dil		Dil H2O	Live Charac	Line Slurry	Lime Slurry	Line Slurry	Dil H2O	Dil H2O
	Water	Discharge	Tank Out	Pump Out	H2O Tank	Return	H2O Tank		Pump Out	to SDA-1	to SDA-2	to SDA-3	to SDA-4	to SDA-1	to SDA-2
lb/min H2O	33.6	69.6	366.5	3/4.8	9.2	296.9	406.1	415.3	415.3	17.2	17.2	17.2	17.2	93.5	93.5
b/min CaO	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
lb/min Ca(OH)2	0.0	20.3	97.6	97.6	2,4	77.3	0.0	2.4	2,4	4.5	4.5	4.5	4.5	0.5	0.5
ib/min CaSO3*1/2H2O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
lb/min CaCl2	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
ib/min CaF2	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
lb/min Inerts	0.0	1.4	6.6	6.6	0.2	5.2	4.1	4.3	4.3	0.3	0.3	0.3	0.3	1.0	1.0
lb/min ash	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
ib/min subtotal solids	0.0	21.6	104.1	104.1	2.6	82.5	4.1	6.7	6.7	4.8	4.8	4.8	4.8	1.5	1.5
lb/min total	33.6	91.2	470.6	479.0	11.8	379.4	410.2	422.0	422.0	22.0	22.0	22.0	22.0	95.0	95.0
wt % moisture	100.0	76.3	0.0	0.0	0.0	0.0	0.0	0.0	6.7	0.0	0.0	0.0	0.0	0.0	0.0
wt% solids	0.0	23.7	22.1	21.7	21.7	21.7	1.0	1.6	422.0	21.7	21.7	21.7	21.7	1.6	1.6
GPM	4.0	9.4	49.0	50.0	1.2	39.6	48.9	50.1	50.1	2.3	2.3	2.3	2.3	11.3	11.3
	Dil H2O	Dil H2O	L1Z.I	Slurry Feed	L12.3	L12.4	DII H2O		14 Contact	Peb Lime	Slaker Grit	Lime Pump	SWZ-EXCESS Lime Pump	Dil Pumo	Strainer
	to SDA-3	ω SDA-4	to SDA-1	to SDA-2				1002	Contact	LCD THUS		PRINC LORIGIN			Flush H2O
n. (:- U2O	m apr-3						l to Claker	u	20	to Cloker	Discharge	Coal H2O	Coal H2O	Coul HOO	
80/m36 M/L)	- 011				to SDA-3	to SDA-4	to Slaker		20	to Slaker	Discharge	Scal H2O	Seal H2O	Seal H2O	11011120
lb/min H2O lb/min CeO	93.5	93.5	710.7	110.7	110.7	110.7	41.4	44	7.5	0.2	0.3	8.3	8.3	U	0
lb/min CaO	0.0	93.5 0.0	710.7 0.0	110.7 0.0	110.7	110.7	41.4	44	7.5 .0	0.2 15.3	0.3 0.0	8.3 0.0	8.3 0.0	Seal H2O 0 0	0
		93.5 0.0 0.5	710.7	0.0 5.0	0.0 5.0	0.0 5.0	41.4 0.0 0.2	44 0 0	7.5 .0 .2	0.2 15.3 0.2	0.3 0.0 0.0	8.3 0.0 0.0	8.3	0	U
lb/min CaO lb/min Ca(OH)2	0.0 0.5	93.5 0.0	710.7 0.0 5.0	110.7 0.0 5.0 0.0	110.7	0.0 5.0 0.0	41.4 0.0 0.2 0.0	44 0 0 0	7.5 .0 .2 .0	0.2 15.3 0.2 15.2	0.3 0.0	8.3 0.0	8.3 0.0 0.0	0	0
lb/min CaO lb/min Ca(OH)2 lb/min CaSO3*1/2H2O	0.0 0.5 0.0	93.5 0.0 0.5 0.0	710.7 0.0 5.0 0.0	0.0 5.0	110.7 0.0 5.0 0.0	0.0 5.0	41.4 0.0 0.2	44 0 0 0 0	7.5 .0 .2	0.2 15.3 0.2	0.3 0.0 0.0 0.0	8.3 0.0 0.0 0.0	8.3 0.0 0.0 0.0	0 0 0	0
lb/min CaO lb/min Ca(OH)2 lb/min CaSO3*1/2H2O lb/min CaCl2	0.0 0.5 0.0 0.0	93.5 0.0 0.5 0.0 0.0	710:7 0.0 5.0 0.0 0.0	110.7 0.0 5.0 0.0	110.7 0.0 5.0 0.0 0.0	110.7 0.0 5.0 0.0 0.0	41.4 0.0 0.2 0.0 0.0	44 0 0 0 0	7.5 .0 .2 .0	0.2 15.3 0.2 15.2 0.0	0.3 0.0 0.0 0.0 0.0	8.3 0.0 0.0 0.0 0.0	8.3 0.0 0.0 0.0 0.0	0 0 0 0	0 0 0
lb/min CeO lb/min Ce(OH)2 lb/min CaSO3*1/2H2O lb/min CeCl2 lb/min CaF2	0.0 0.5 0.0 0.0 0.0	93.5 0.0 0.5 0.0 0.0	710.7 0.0 5.0 0.0 0.0	0.0 5.0 0.0 0.0 0.0	110.7 0.0 5.0 0.0 0.0	0.0 5.0 0.0 0.0 0.0	41.4 0.0 0.2 0.0 0.0 0.0	44 0 0 0 0 0 0	7.5 .0 .2 .0 .0	0.2 15.3 0.2 15.2 0.0 0.0	0.3 0.0 0.0 0.0 0.0 0.0	8.3 0.0 0.0 0.0 0.0 0.0	8.3 0.0 0.0 0.0 0.0 0.0	0 0 0 0	0 0 0 0
lb/min CeO lb/min Ce(OH)2 lb/min CaSO3*1/2H2O lb/min CeCl2 lb/min CaF2 lb/min Inerts	0.0 0.5 0.0 0.0 0.0 1.0	93.5 0.0 0.5 0.0 0.0 0.0	0.0 5.0 0.0 0.0 0.0 1.3	0.0 5.0 0.0 0.0 0.0 1.3	0.0 5.0 0.0 0.0 0.0 0.0	0.0 5.0 0.0 0.0 0.0 0.0	41.4 0.0 0.2 0.0 0.0 0.0 0.0	44 0 0 0 0 0 0 0 4	7.5 .0 .2 .0 .0 .0	0.2 15.3 0.2 15.2 0.0 0.0	0.3 0.0 0.0 0.0 0.0 0.0 1.0	8.3 0.0 0.0 0.0 0.0 0.0	8.3 0.0 0.0 0.0 0.0 0.0 0.0	0 0 0 0 0	0 0 0
lb/min CeO lb/min Ce(OH)2 lb/min CaSO3*1/2H2O lb/min CeCl2 lb/min CaF2 lb/min Inerts lb/min ash	0.0 0.5 0.0 0.0 0.0 1.0	93.5 0.0 0.5 0.0 0.0 0.0 1.0	0.0 5.0 0.0 0.0 0.0 1.3	0.0 5.0 0.0 0.0 0.0 1.3	0.0 5.0 0.0 0.0 0.0 0.0 1.3	0.0 5.0 0.0 0.0 0.0 1.3	41.4 0.0 0.2 0.0 0.0 0.0 0.4 0.0	44 0 0 0 0 0 0 4	7.5 .0 .2 .0 .0 .0 .0 .5	0.2 15.3 0.2 15.2 0.0 0.0 1.9	0.3 0.0 0.0 0.0 0.0 0.0 1.0	8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 8.3	8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 8.3	0 0 0 0 0	0 0 0 0 0 0
lb/min CaO lb/min Ca(OH)2 lb/min CaSO3°1/2H2O lb/min CaCl2 lb/min CaF2 lb/min Inerts lb/min ash lb/min subtotal solids	0.0 0.5 0.0 0.0 0.0 1.0 0.0	93.5 0.0 0.5 0.0 0.0 0.0 1.0 0.0	0.0 5.0 0.0 0.0 0.0 1.3 0.0 6.3	0.0 5.0 0.0 0.0 0.0 1.3 0.0 6.3	0.0 5.0 0.0 0.0 0.0 1.3 0.0 6.3	0.0 5.0 0.0 0.0 0.0 1.3 0.0 6.3	41.4 0.0 0.2 0.0 0.0 0.0 0.4 0.0 0.6	44 0 0 0 0 0 0 0 4 4 0 45	7.5 .0 .2 .0 .0 .0 .5 .0	0.2 15.3 0.2 15.2 0.0 0.0 1.9 0.0 17.3	0.3 0.0 0.0 0.0 0.0 0.0 1.0 0.0	8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0	8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
lb/min CaO lb/min Ca(OH)2 lb/min CaSO3*1/2H2O lb/min CaCl2 lb/min CaF2 lb/min Inerts lb/min ash lb/min subtotal solids lb/min total	0.0 0.5 0.0 0.0 0.0 1.0 0.0 1.5 95.0	93.5 0.0 0.5 0.0 0.0 0.0 1.0 0.0 1.5	0.0 5.0 0.0 0.0 0.0 1.3 0.0 6.3	110.7 0.0 5.0 0.0 0.0 0.0 1.3 0.0 6.3 116.9	110.7 0.0 5.0 0.0 0.0 0.0 1.3 0.0 6.3 116.9	110.7 0.0 5.0 0.0 0.0 0.0 1.3 0.0 6.3	41.4 0.0 0.2 0.0 0.0 0.0 0.4 0.0 0.6 42.0	44 0 0 0 0 0 0 4 4 0 45 98	7.5 0 2 .0 .0 .0 .5 .0 .8 2.2	0.2 15.3 0.2 15.2 0.0 0.0 1.9 0.0 17.3 17.4	0.3 0.0 0.0 0.0 0.0 0.0 1.0 0.0 1.0	8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 8.3	8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 8.3	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 0 0 0 0 0



WHEELABRATOR MCKAY BAY APC RETROFIT PROJECT

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Table 2.1.2 Dry Scrubbing System Mass Balance 100% MCR: 80%EA: Dirty Boiler: 90% UCL

		100% MCR;	80%EA; Dirt	y Boiler; 90%	UCL			
	Fl	F2	F3	F4	F5	F6	S3	S4
	SDA	SDA	SDA	SDA	FF	FF	SDA	FF
	Inlet	Inleak	Atom Air	Out	Leak	Out	Discharge	Discharge
lb/min CO2	339.4	0.0	0.0	339.4	0.0	339.4	0.0	0.0
lb/min O2	221.6	11.9	6.0	239.5	13.6	253.1	0.0	0.0
lb/min N2	1,635.0	39.4	19.7	1,694.1	45.0	1,739.2	0.0	0.0
lb/min H2O	246.4	0.7	0.3	358.0	0.8	358.7	0.1	0.1
lb/min SO2	1.17	0.00	0.00	0.35	0.00	0.23	0.00	0.00
lb/min HCl	2.17	0.00	0.00	0.22	0.00	0.11	0.00	0.00
lb/min HF	0.04	0.00	0.00	0.00	0.00	0.00	0.00	0.00
lb/min SO3	0.05	0.00	0.00	0.05	0.00	0.01	0.00	0.00
lb/min subtotal fluegas	2,445.8	52.0	26.0	2,631.6	59.4	2,690.8	0.0	0.0
lb/min Ca(OH)2	0.0	0.0	0.0	1.6	0.0	0.0	0.4	1.3
lb/min CaSO3*1/2H2O	0.0	0.0	0.0	1.3	0.0	0.0	0.3	1.6
lb/min CaCl2	0.0	0.0	0.0	2.4	0.0	0.0	0.6	2.5
In/min CaF2	0.0	0.0	0.0	0.1	0.0	0.0	0.0	0.1
in Inerts	0.0	0.0	0.0	0.8	0.0	0.0	0.2	0.8
lo min ash	8.8	0.0	0.0	7.0	0.0	0.0	1.8	7.0
lb/min subtotal solids	8.8	0.0	0.0	13.1	0.0	0.0	3.4	13.3
lb/min total	2454.6	52.0	26.0	2644.8	59.4	2690.8	3.4	13.4
SCFM	33,454	. 701	350	36,846	801	37,645	0	0
SDCFM	28,177	686	343	29,180	784	29,962	0	0
ACFM	60,672	691	60	52,842	789	54,532	0	0
vol % CO2	8.89	0.00	0.00	8.07	0.00	7.90	0.00	0.00
vol % O2	7.98	20.50	20.50	7.83	20.50	8.10	0.00	0.00
vol % N2	67.27	77.40	77.40	63.29	77.40	63.59	0.00	0.00
vol % H2O	15.77	2.10	2.10	20.81	2.10	20.41	0.00	0.00
ppm (v-wgb) SO2	210	0	0	57	0	37	0	0
ppm (v-wgb) HCl	684	0	0	62	0	30	0	0
ppm (v-wgb) HF	24	0	0	2	. 0	2	0	0
ppm (v-wgb) SO3	7	0	0	7	0	1	0	0
gr/scf	1.831	0.000	0.000	2.492	0.000	0.006	0.000	0.000
gr/acf	1.010	0.000	0.000	1.738	0.000	0.004	0.000	0.000
ppm (v-dgb) SO2 @7% O2	303	0	0	91	0	61	0	0
ppm (v-dgb) HCl @7% O2	988	0	0	99	0	49	0	0
ppm (v-dgb) HF @7% O2	34	0	0	3	0	3	0	0
ppm (v-dgb) SO3 @7% O2	10	0	0	10	0	1	0	0
gr/sdcf @7% O2	2.644	0.000	0.000	3.971	0.000	0.010	0.000	0.000
deg F	489	60	120	285	60	277	0	0
deg F	148	66	87	147	20	146	20	0
rdp deg F	130	65	65	141	19	140	19	0
Pa (in Hg)	29.65	29.90	192.73	29.44	29.90	28.85	0.00	0.00
Ps (in Wg)	-3.30	0.00	0.00	-6.15	0.00	-14.15	0.00	0.00



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WHEELABRATOR MCKAY BAY

APC RETROFIT PROJECT

Absorbent Preperation System Mass Balance

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Boiler # 1; Case # 9; 100% MCR; 80%EA; Clean Boiler; 50% UCL Boiler # 2; Case # 9; 100% MCR; 80%EA; Clean Boiler; 50% UCL Boiler # 3; Case # 9; 100% MCR; 80%EA; Clean Boiler; 50% UCL Boiler # 4; Case # 9; 100% MCR; 80%EA; Clean Boiler; 50% UCL

		12/	LJ	LA T	E3	L8	L/	1.8	Ly	LIU.I	L10.2	L10.5	L10.4	a din m	131.2
	Slaker	Slaker	Lime	Lime		Lime Pump			Dil H2O	Lime Slurry		Lime Slurry	Lime Slurry	Dil H2O	Dil H2O
	Water	Discharge	Tank Out	Pump Out	H2O Tank	Return			Pump Out	to SDA-I	to SDA-2	to SDA-3	to SDA-4	to SDA-1	to SDA-2
lb/min H2O	20.2	41.8	369.1	311.4	5.5	321.2	285.0	292.5	292.5	10.9	10.9	10.9	10.9	66.9	66.9
lb/min CaO	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
b/min Ca(OH)2	0.0	12.2	91.7	91.7	1.6	79.5	0.0	1.6	1.6	2.7	2.7	2.7	2.7	0.4	0.4
b/min CaSO3*1/2H2O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
lb/min CaCl2	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
lb/min CaF2	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
lb/min Inerts	0.0	0.8	6.2	6.2	0.1	5.4	2.9	3.0	3.0	0.2	0.2	0.2	0.2	0.7	0.7
lb/min ash	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
lb/min subtotal solids	0.0	13.0	97.9	97.9	1.7	84.9	2.9	4.6	4.6	2.8	2.8	2.8	2.8	1.1	1.1
lb/min total	20.2	54.8	467.0	475.3	8.2	412.1	288.9	297.0	297.0	13.8	13.B	13.8	13.8	67.9	67.9
wt % moisture	100.0	76.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
wt% solids	0.0	23.7	21.0	20.6	20.6	20.6	1.0	1.5	1.5	20.6	20.6	20.6	20.6	1.5	1.5
GPM	2.4	5.6	49.0	50.0	0.9	43.4	34.4	35.3	35.3	1.4	1.4	1.4	1.4	8.1	8.1
***************************************	L11.3	L11.4	L12.1	£12.2	L12.3	L12.4	L13	L14	LIS	31	52		3WZ-EXCESS	2M2	3 W4-111141
	Dil H2O	Dil H2O		Slurry Feed	Slurry Feed	Slurry Feed	Dil H2O	Total	Lime Slurry	Peb Lime	Grit	Lime Pump		Dil Pump	Strainer
	to SDA-3	ဖ SDA-4	to SDA-1	to SDA-2	to SDA-3	to SDA-4	to Slaker	H2O	to Ash cond.	to Slaker	Discharge	Seal H2O	Seal H2O	Seal H2O	Flush H20
lb/min H2O	66.9	66.9	11.8	77.8	77.8	77.8	24.9	310.8	22.2		0.2	8.3	8.3	0.0	0.
lb/min CaO	0.0	0.0	0.0	0.0	0.0	0.0	0.0					0.0	0.0		0.0
lb/min Ca(OH)2	0.4	0.4	3.0	3.0	3.0	3.0	0.1	0.1	6.5		0.0	0.0	0.0	• • •	0.0
lb/min CaSO3*1/2H2O	0.0	0.0	0.0	0.0	0.0	0.0	0.0				0.0	0.0	0.0		0.0
lb/min CaCl2	0.0	0.0	0.0	0.0	0.0	0.0	0.0		1		0.0	0.0	0.0		0.0
lb/min CaF2	0.0	0.0	0.0	0.0	0.0	0.0	0.0				0.0	0.0	0.0		0.0
lb/min Inerts	0.7	0.7	0.9	0.9	0.9	0.9	0.3					0.0	0.0		0.0
lb/min ash	0.0	0.0	0.0	0.0	0.0	0.0	0.0				0.0	0.0	0.0	***	0.0
lb/min subtotal solids	1.1	1.1	3.9	3.9	3.9	3.9	0.4					0.0	0.0		0.0
lb/min total	67.9	67.9	81.7	81.7	81.7	81.7	25.2	314.1				8.3	8.3		0.0
wt % moisture	0.0	0.0	0.0	0.0	0.0	0.0	98.5					0.0	0.0		0.0
wt% solids	1.5	1.5	4.8	4.8	4.8	4.8	1.5	2.5	23.7	99.0	75.0	0.0	0.0	100.0	100.
GPM	8.1	8.1	9.5	9.5	9.5	9.5	3.0	37.4	3.0	0.0	0.0	1.0	1.0	0.0	0.0

City of Tampa O & M N McKay Bay Refuse to Energy Facility Retrofit Project

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WHEELABRATOR MCKAY BAY

APC RETROFIT PROJECT

WAPC CONTRACT 3834 MARCH 26, 1999

Table 2.1.2 Dry Scrubbing System Mass Balance

100% MCR; 80%EA; Clean Boller; 50% UCL												
	FI	F2	F3	F4	F5	F6	S3	S4				
	SDA	SDA	SDA	SDA	FF	FF	SDA	FF				
	Inlet	inicak	Atom Air	Out	Leak	Out	Discharge	Discharge				
lb/min CO2	339.4	0.0	0.0	339.4	0.0	339.4	0.0	0.0				
lb/min O2	221.6	11.9	6.0	239.5	13.6	253.1	0.0	0.0				
lb/min N2	1,635.0	39.4	19.7	1,694.1	45.0	1,739.2	0.0	0.0				
lb/min H2O	246.4	0.7	0.3	325.2	0.8	325.9	0.1	0.1				
lb/min SO2	0.67	0.00	0.00	0.20	0.00	0.13	0.00	0.00				
lb/min HCl	1.33	0.00	0.00	0.13	0.00	0.07	0.00	0.00				
lb/min HF	0.04	0.00	0.00	0.00	0.00	0.00	0.00	0.00				
lb/min SO3	0.05	0.00	0.00	0.05	0.00	0.01	0.00	0.00				
lb/min subtotal fluegas	2,444.5	52.0	26.0	2,598.6	59.4	2,657.8	0.0	0.0				
lb/min Ca(OH)2	0.0	0.0	0.0	1.0	0.0	0.0	0.2	0.8				
lb/min CaSO3*1/2H2O	0.0	0.0	0.0	0.8	0.0	0.0	0.2	1.0				
lb/min CaCl2	0.0	0.0	0.0	1.4	0.0	0.0	0.4	1.5				
lb/min CaF2	0.0	0.0	0.0	0.1	0.0	0.0	0.0	0.1				
lb/min Inerts	0.0	0.0	0.0	0.6	0.0	0.0	0.1	0.6				
lb/min ash	8.8	0.0	0.0	7.0	0.0	0.0	1.8	7.0				
b/min subtotal solids	8.8	0.0	0.0	10.8	0.0	0.0	2.8	10.9				
b/min total	2453.3	52.0	26.0	2609.3	59.4	2657.9	2.8	11.0				
SCFM	33,442	701	350	36,141	801	36,941	0	0				
SDCFM	28,165	686	343	29,178	784	29,961	0	0				
ACFM	56,849	691	60	51,686	789	53,347	0	0				
vol % CO2	8.89	0.00	0.00	8.23	0.00	8.05	0.00	0.00				
vol % O2	7.98	20.50	20.50	7.98	20.50	8.25	0.00	0.00				
vol % N2	67.30	77.40	77.40	64.52	77.40	64.80	0.00	0.00				
vol % H2O	15.78	2.10	2.10	19.27	2.10	18.89	0.00	0.00				
ppm (v-wgb) SO2	120	0	0	33	0	22	0	0				
ppm (v-wgb) HCl	421	0	0	39	0	19	0	0				
ppm (v-wgb) HF	24	0	0	2	0	2	0	0				
ppm (v-wgb) SO3	7	0	0	7	0	1	0	0				
gr/scf	1.832	0.000	0.000	2.085	0.000	0.006	0.000	0.000				
gr/acf	1.077	0.000	0.000	1.458	0.000	0.004	0.000	0.000				
ppm (v-dgb) SO2 @7% O2	173	0	0	52	0	35	0	0				
ppm (v-dgb) HCl @7% O2	608	0	0	61	0	30	0	0				
ppm (v-dgb) HF @7% O2	34	0	0	3	0	3	0	0				
ppm (v-dgb) SO3 @7% O2	10	o	0	10	0	1	0	0				
gr/sdcf @7% O2	2.646	0.000	0.000	3.260	0.000	0.010	0.000	0.000				
Tdb deg F	432	60	120	285	60	277	0	0				
Twb deg F	146	66	87	144	20	144	20	0				
Tdp deg F	130	65	65	138	19	137	19	0				
Pa (in Hg)	29.73	29.90	192.73	29.52	29.90	28.93	0.00	0.00				
Ps (in Wg)	-2.20	0.00	0.00	-5.05	0.00	-13.05	0.00	0.00				
			0,00									



Wheelabrator Air Pollution Control Pittsburgh, Pennsylvania 1-800-327-8727 www.wapc.com

City of Tampa McKay Bay Refu Retrofit Project

Energy Facility

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WHEELABRATOR MCKAY BAY

APC RETROFIT PROJECT

WAPC CONTRACT 3834 MARCH 26, 1999

Absorbent Preparation System Mass Balance

Boiler # 1; Case # 15; 100% MCR; 80%EA; Dirry Boiler; 50% UCL; SDA Off-Line Boiler # 2; Case # 15; 100% MCR; 80%EA; Dirry Boiler; 50% UCL; SDA Off-Line Boiler # 3; Case # 8; 100% MCR; 80%EA; Dirry Boiler; 90% UCL Boiler # 4; Case # 8; 100% MCR; 80%EA; Dirry Boiler; 90% UCL

	Slaker	Slaker	Lime	L4 Lime	L3	Lime Pump	L/	La Dil H2O	L9 Dil H2O	LIV.1 Lime Shurry	L10.2 Lime Slurry	Line Sturry	Line Sturry	Dil H2O	Dil H2O
	Water	Discharge	Tank Out	Pump Out	H2O Tank	Return	H2O Tank	Tank Out	Pump Out	to SDA-1	to SDA-2	to SDA-3	to SDA-4	to SDA-1	to SDA-2
lb/min H2O	16.8	34.8	370.1	378.5	4.5	335.4	198.9	203.4	203.4	0.0	0.0	7.1	7:1	0.0	0.0
lb/min CaO	0.0	0.0		0.0	0.0		0.0	0.0	0.0		0.0			0.0	0.0
lb/min Ca(OH)2	0.0	10.1			1.1	78.9	0.0	1.1	1.1	0.0	0.0		1.7	0.0	0.0
1b/min CaSO3*1/2H2O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0		0.0	0.0	0.0	0.0	0.0
lb/min CaCl2	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
lb/min CaF2	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
lb/min inerts	0.0		6.0	6.0	0.1	5.3	2.0	2.1	2.1	0.0	0.0		0.1	0.0	0.0
lb/min ash	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
lb/min subtotal solids	0.0	10.8	95.0	95.0	1.1	84.2	2.0	3.2	3.2	0.0	0.0	1.8	1.8	0.0	0.0
lb/min total	16.8	45.6	465.1	473.5	5.7	419.5	200.9	206.5	206.5		0.0	8.9	8.9	0.0	0.0
wt % moisture	100.0	76.3		0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
wt% solids	0.0	23.7	20.4	20.1	20.1	20.1	1.0	1.5	1.5	0.0	0.0	20.1	20.1	0.0	0.0
GPM	2.0	4.7	49.0	50.0	0.6	44.3	24.0	24.6	24.6	0.0	0.0	0.9	0.9	0.01	0.0
	THE R. P. LEWIS CO., LANSING	delegation of the same				***************************************				L					
	E11.5	E11.4	L12.1	L12.2 Slurny Food	L12.3	L12.4	LI3	L14	Libe Sheer	SI Peh Lime	SZ Grit		SW2-Excess		Strainer
	Dil H2O	Dil H2O	Slurry Feed	Slurry Feed	Slurry Feed	Slurry Feed	Dil H2O	L14 Total Contact	Lime Slurry	Peb Lime	Grit	Lime Pump	SW2-Excess Lime Pump Seal H2O	SW3 Dit Pump Seal H2O	Strainer Flush H2O
lb/min H2O	Dil H2O	Dil H2O		Slurry Feed to SDA-2	Slurry Feed to SDA-3		Dil H2O to Slaker	L14 Total Contact H2O	Lime Slurry to Ash cond.				Lime Pump	Dil Pump	Strainer
lb/min H2O lb/min CaO	Dil H2O to SDA-3	Dil H2O to SDA-4 103.5	Slurry Feed to SDA-1	Slurry Feed	Slurry Feed to SDA-3	Sturry Feed to SDA-4	Dil H2O	L14 Total Contact H2O 219.6	Lime Slurry to Ash cond. 22.2	Peb Lime to Slaker	Grit Discharge	Lime Pump Seal H2O	Lime Pump Seal H2O	Dil Pump Seal H2O	Strainer
	Dil H2O to SDA-3 103.5	Dil H2O to SDA-4 103.5 0.0	Slurry Feed to SDA-1 0.0	Slurry Feed to SDA-2 0.0 0.0	Slurry Feed to SDA-3	Sturry Feed to SDA-4 110.7 0.0	Dil H2O to Slaker 20.7	L14 Total Contact H2O	Lime Slurry to Ash cond. 22.2	Peb Lime to Slaker U.1	Grit Discharge 0.2	Lime Pump Seal H2O 8.3 0.0	Lime Pump Seal H2O 8.3 0.0	Dil Pump Scal H2O 0.0	Strainer Flush H2O 0.0
lb/min CaO	Dil H2O to SDA-3 103.5 0.0	Dil H2O to SDA-4 103.5 0.0 0.5	Slurry Feed to SDA-1 0.0 0.0	Siurry Feed to SDA-2 0.0 0.0 0.0	Slurry Feed to SDA-3 110.7 0.0 2.2	Sturry Feed to SDA-4 110.7 0.0	Dil H2O to Slaker 20.7 0.0 0.1	Total Contact H2O 219.6 0.0	Lime Slurry to Ash cond. 22:2 0.0 6.5	Peb Lime to Slaker U.1 7.6	Grit Discharge 0.2 0.0 0.0	Lime Pump Seal H2O 8.3 0.0 0.0 0.0	Lime Pump Seal H2O 8.3 0.0 0.0 0.0	Dil Pump Scal H2O 0.0 0.0	Strainer Flush H2O 0.0 0.0 0.0
lb/min CaO lb/min Ca(OH)2 lb/min CaSO3*1/2H2O lb/min CaCl2	Dil H2O to SDA-3 103.5 0.0 0.5	Dil H2O to SDA-4 103.5 0.0 0.5 0.0	Slurry Feed to SDA-1 0.0 0.0 0.0 0.0 0.0	Slurry Feed to SDA-2 0.0 0.0 0.0 0.0	Slurry Feed to SDA-3 110.7 0.0 2.2	Slurry Feed to SDA-4 110.7 0.0 2.2	Dil H2O to Slaker 20.7 0.0 0.1	Total Contact H2O 219.6 0.0 0.1	Lime Slurry to Ash cond. 22.2 0.0 6.5 0.0	Peb Lime to Slaker 0.1 7.6 0.0	Grit Discharge 0.2 0.0 0.0 0.0 0.0	Lime Pump Seal H2O 8.3 0.0 0.0 0.0	Lime Pump Seal H2O 8.3 0.0 0.0 0.0	Dil Pump Scal H2O 0.0 0.0	Strainer Flush H2O 0.0 0.0 0.0 0.0
lb/min CaO lb/min Ca(OH)2 lb/min CaSO3*1/2H2O lb/min CaCl2 lb/min CaF2	Dil H2O to SDA-3 103.5 0.0 0.5 0.0 0.0	Dil H2O to SDA-4 103.5 0.0 0.5 0.0	Slurry Feed to SDA-1 0.0 0.0 0.0 0.0 0.0 0.0	Slurry Feed to SDA-2 0.0 0.0 0.0 0.0	Slurry Feed to SDA-3 110.7 0.0 2.2 0.0	Sturry Feed to SDA-4 110.7 0.0 2.2 0.0	Dil H2O to Slaker 20.7 0.0 0.1 0.0 0.0	L14 Total Contact H2O 219.6 0.0 0.1 0.0	Lime Slurry to Ash cond. 22.2 0.0 6.5 0.0 0.0	Peb Lime to Slaker 0.1 7.6 0.0 0.0 0.0 0.0	Grit Discharge 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Lime Pump Seal H2O 8.3 0.0 0.0 0.0 0.0 0.0	Eime Pump Seal H2O 8.3 0.0 0.0 0.0 0.0 0.0	Dit Pump Scal H2O 0.0 0.0 0.0 0.0 0.0	Strainer Flush H2O 0.0 0.0 0.0 0.0 0.0 0.0
lb/min CaO lb/min Ca(OH)2 lb/min CaSO3*1/2H2O lb/min CaCl2 lb/min CaF2 lb/min lnerts	Dil H2O to SDA-3 103.5 0.0 0.5 0.0 0.0 0.0	Dil H2O to SDA-4 103.5 0.0 0.5 0.0 0.0 0.0 1.1	Sturry Feed to SDA-1 0.0 0.0 0.0 0.0 0.0 0.0	Siurry Feed to SDA-2 0.0 0.0 0.0 0.0 0.0	Sturry Feed to SDA-3 110.7 0.0 2.2 0.0 0.0 0.0 1.2	Sturry Feed to SDA-4 110.7 0.0 2.2 0.0 0.0 0.0 1.2	Dil H2O to Slaker 20.7 0.0 0.1 0.0 0.0 0.0 0.0	E14 Total Contact H2O 219.6 0.0 0.1 0.0 0.0 0.0 0.0 2.2	Lime Slurry to Ash cond. 22:2 0.0 6.5 0.0 0.0 0.0 0.0	Peb Lime to Slaker 0.1 7.6 0.0 0.0 0.0 0.0 0.0	Grit Discharge 0.0 0.0 0.0 0.0 0.0 0.0	Lime Pump Seal H2O 8.3 0.0 0.0 0.0 0.0 0.0 0.0	Lime Pump Seal H2O 8.3 0.0 0.0 0.0 0.0 0.0 0.0	Dit Pump Seal H2O 0.0 0.0 0.0 0.0 0.0 0.0	Strainer Flush H2O 0.0 0.0 0.0 0.0 0.0 0.0 0.0
lb/min CaO lb/min Ca(OH)2 lb/min CaSO3*1/2H2O lb/min CaCl2 lb/min CaF2 lb/min lnerts lb/min ash	Dil H2O to SDA-3 103.3 0.0 0.5 0.0 0.0 0.0 1.1 0.0	Dil H2O to SDA-4 103.5 0.0 0.5 0.0 0.0 0.0 1.1 0.0	Slurry Feed to SDA-1 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Sturry Feed to SDA-2 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Slurry Feed to SDA-3 110.7 0.0 2.2 0.0 0.0 0.0 1.2 0.0	Slurry Feed to SDA-4 110.7 0.0 2.2 0.0 0.0 0.0 1.2	Dil H2O to Slaker 20.7 0.0 0.1 0.0 0.0 0.0 0.0 0.2	114 Total Contact H2O 219.6 0.0 0.1 0.0 0.0 0.0 0.0 2.2	Lime Slurry to Ash cond. 22.2 0.0 6.5 0.0 0.0 0.0 0.4	Peb Lime to Staker 0.1 7.6 0.0 0.0 0.0 0.0 0.0 0.9	Grit Discharge 0.2 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Lime Pump Seal H2O 8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Lime Pump Seal H2O 8.3 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Strainer Flush H2O 0.0 0.0 0.0 0.0 0.0 0.0 0.0
Ib/min CaO Ib/min Ca(OH)2 Ib/min CaSO3*1/2H2O Ib/min CaC12 Ib/min CaF2 Ib/min Inerts Ib/min ash Ib/min subtotal solids	Dil H2O to SDA-3 103.3 0.0 0.5 0.0 0.0 0.0 1.1 0.0 1.6	Dil H2O to SDA-4 103.5 0.0 0.5 0.0 0.0 0.0 1.1 0.0	Slurry Feed to SDA-1 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Siurry Feed to SDA-2 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Sturry Feed to SDA-3 110.7 0.0 2.2 0.0 0.0 0.0 1.2	Sturry Feed to SDA-4 110.7 0.0 2.2 0.0 0.0 0.0 1.2 0.0 3.4	Dil H2O to Slaker 20.7 0.0 0.1 0.0 0.0 0.0 0.0 0.2 0.0	114 Total Contact H2O 219.6 0.0 0.1 0.0 0.0 0.0 2.2 0.0 2.3	Lime Slurry to Ash cond. 22.2 0.0 6.5 0.0 0.0 0.0 0.4 0.0 6.9	Peb Lime to Slaker 0.1 7.6 0.0 0.0 0.0 0.0 0.0 0.9 0.0 8.5	Grit Discharge 0.2 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.5 0.0 0.5	Lime Pump Seal H2O 8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Lime Pump Seal H2O 8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Dit Pump Seal H2O 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Strainer Flush H2O 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
Ib/min CaO Ib/min Ca(OH)2 Ib/min CaSO3*1/2H2O Ib/min CaC12 Ib/min CaF2 Ib/min Inerts Ib/min ash Ib/min subtotal solids Ib/min total	Dil H2O to SDA-3 103.5 0.0 0.5 0.0 0.0 1.1 0.0 1.6 105.1	Dil H2O to SDA-4 103.5 0.0 0.5 0.0 0.0 0.0 1.1 0.0 1.6 105.1	Slurry Feed to SDA-1 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Siurry Feed to SDA-2 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	Slurry Feed to SDA-3 110.7 0.0 2.2 0.0 0.0 0.0 1.2 0.0 3.4 114.0	Sturry Feed to SDA-4 110.7 0.0 2.2 0.0 0.0 0.0 1.2 0.0 3.4	Dil H2O to Slaker 20:7 0.0 0.1 0.0 0.0 0.0 0.2 0.0 0.3 21.0	L14 Total Contact H2O 219.6 0.0 0.1 0.0 0.0 0.0 2.2 0.0 2.3 221.9	Lime Slurry to Ash cond. 22.2 0.0 6.5 0.0 0.0 0.0 0.4 0.0 6.9 29.1	Peb Lime to Slaker 0.1 7.6 0.0 0.0 0.0 0.0 0.9 0.0 8.5 8.6	Grit Discharge 0.2 0.0 0.0 0.0 0.0 0.0 0.0 0.5 0.0 0.5	Lime Pump Seal H2O 8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0	Lime Pump Seal H2O 8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Dit Pump Seal H2O 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Strainer Flush H2O 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
Ib/min CaO Ib/min Ca(OH)2 Ib/min CaSO3*1/2H2O Ib/min CaC12 Ib/min CaF2 Ib/min Inerts Ib/min ash Ib/min subtotal solids Ib/min total wt % moisture	Dil H2O to SDA-3 103.5 0.0 0.5 0.0 0.0 1.1 0.0 1.6 105.1	Dil H2O to SDA-4 103.5 0.0 0.5 0.0 0.0 0.0 1.1 0.0 1.6 105.1	Slurry Feed to SDA-1 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	Slurry Feed to SDA-2 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	Slurry Feed to SDA-3 110.7 0.0 2.2 0.0 0.0 0.0 1.2 0.0 3.4 114.0	Sturry Feed to SDA-4 110.7 0.0 2.2 0.0 0.0 1.2 0.0 3.4 114.0 0.0	Dil H2O to Slaker 20:7 0.0 0.1 0.0 0.0 0.0 0.2 0.0 0.3 21.0 98.5	Total Contact H2O 219.6 0.0 0.1 0.0 0.0 0.0 2.2 0.0 2.3 221.9 98.5	Lime Slurry to Ash cond. 22.2 0.0 6.5 0.0 0.0 0.0 0.4 0.0 6.9 29.1	Peb Lime to Slaker 0.1 7.6 0.0 0.0 0.0 0.0 0.9 0.0 8.5 8.6 1.0	Grit Discharge 0.2 0.0 0.0 0.0 0.0 0.0 0.5 0.0 0.5 0.6 25.0	Lime Pump Seal H2O 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	Lime Pump Seal H2O 8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	Dit Pump Seal H2O 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	Strainer Flush H2O 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.
Ib/min CaO Ib/min Ca(OH)2 Ib/min CaSO3*1/2H2O Ib/min CaC12 Ib/min CaF2 Ib/min Inerts Ib/min ash Ib/min subtotal solids Ib/min total	Dil H2O to SDA-3 103.5 0.0 0.5 0.0 0.0 1.1 0.0 1.6 105.1	Dil H2O to SDA-4 103.5 0.0 0.5 0.0 0.0 0.0 1.1 0.0 1.55.1 0.0	Slurry Feed to SDA-1 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	Siurry Feed to SDA-2 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	Slurry Feed to SDA-3 110.7 0.0 2.2 0.0 0.0 0.0 1.2 0.0 3.4 114.0	Sturry Feed to SDA-4 110.7 0.0 2.2 0.0 0.0 0.0 1.2 0.0 3.4	Dil H2O to Slaker 20.7 0.0 0.1 0.0 0.0 0.2 0.0 0.3 21.0 98.5	L14 Total Contact H2O 219.6 0.0 0.1 0.0 0.0 0.0 2.2 0.0 2.3 221.9	Lime Slurry to Ash cond. 22.2 0.0 6.5 0.0 0.0 0.0 0.4 0.0 6.9 29.1	Peb Lime to Staker 0.1 7.6 0.0 0.0 0.0 0.0 0.9 0.0 8.5 8.6 1.0	Grit Discharge 0.2 0.0 0.0 0.0 0.0 0.0 0.0 0.5 0.0 0.5	Lime Pump Seal H2O 8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0	Lime Pump Seal H2O 8.3 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0	Dit Pump Seal H2O 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	Strainer Flush H2O 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.

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Table 2.1.2 Dry Scrubbing System Mass Balance

	FI	MCR; 80%EA	F3	F4	F5	F6	S3	Š4
			SDA	SDA		FF .	SDA	FF
·	SDA	SDA		Out	FF	Out	Discharge	Discharge
11	Iniet	Inleak	Atom Air	339.4	Leak 0.0	339.4	0.0	0.0
lb/min CO2	339.4	0.0	0.0	233.5	13.6	247.1	0.0	0.0
1b/min O2	221.6	11.9 39.4	0.0 0.0	1,674.4	45.0	1,719.5	0.0	0.0
lb/min N2	1,635.0 246.4	0.7	0.0	247.1	0.8	247.8	0.0	0.1
lb/min H2O	0.67	0.00	0.00	0.67	0.00	0.67	0.00	0.00
lb/min SO2	1.33	0.00	0.00	1.33	0.00	1.33	0.00	0.00
lb/min HCl	0.04	0.00	0.00	0.04	0.00	0.04	0.00	0.00
lb/min HF	•	0.00	0.00	0.04	0.00	0.05	0.00	0.00
lb/min SO3	0.05			1	59.4	2,555.9	0.00	0.0
lb/min subtotal fluegas	2,444.5	52.0	0.0	2,496.5	1 .		0.0	0.0
lb/min Ca(OH)2	0.0	0.0	0.0	0.0	0.0	0.0	ll .	1
lb/min CaSO3*1/2H2O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
lb/min CaCl2	0.0	0.0	0.0	0.0	0.0	0.0	0.0	1
lb/min CaF2	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
hh/min Inerts	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
min ash	8.8	0.0	0.0	7.0	0.0	0.0	1.8	7.0
no/min subtotal solids	8.8	0.0	0.0	7.0	0.0	0.0	1.8	
lb/min total	2453.3	52.0	0.0	2503.5	59.4	2556.0	1.8	7.0
SCFM	33,442	701	0	34,142	801	34,942	0	
SDCFM	28,165	686	0	28,851	784	29,635	0	
ACFM	60,651	691	0	61,319	789	63,033	0	0
vol % CO2	8.89	0.00	0.00	8.71	0.00	8.51	0.00	0.00
vol % O2	7.98	20.50	0.00	8.24	20.50	8.52	0.00	0.00
vol % N2	67.30	77.40	0.00	67.51	77.40	67.73	0.00	0.00
vol % H2O	15.78	2.10	0.00	15.49	2.10	15.19	0.00	0.00
ppm (v-wgb) SO2	120	0	0	118	0	115	0	
ppm (v-wgb) HCl	421	0	0	412	0	403	.0	(
ppm (v-wgb) HF	24	0	0	23	0	23	0	(
ppm (v-wgb) SO3	7	0	0	7	0	7	0	C
gr/scf	1.832	0.000	7000.000	1.435	0.000	0.007	0.000	0.000
gr/acf	1.010	0.000	7000.000	0.799	0.000	0.004	0.000	0.000
ppm (v-dgb) SO2 @7% O2	173	0	0	174	0	174	0	C
ppm (v-dgb) HCl @7% O2	608	0	0	608	0	608	0	0
ppm (v-dgb) HF @7% O2	34	0	0	34	0	34	0] 0
ppm (v-dgb) SO3 @7% O2	10	0	0	10	0	10	0	
gr/sdcf @7% O2	2.646	0.000	0.000	2.117	0.000	0.010	0.000	0.000
Tdb deg F	489	60	120	473	60	458	0	0
Twb deg F	148	66	0	147	20	146	20	0
tp deg F	130	65	0	130	19	129	19	0
(in Hg)	29.65	29.90	192.73	29.44	29.90	28.85	0.00	0.00
Ps (in Wg)	-3.30	0.00	0.00	-6.15	0.00	-14.15	0.00	0.00



2.2 Spray Dryer Absorber

Flue gas enters the top of each Spray Dryer Absorber (SDA) through a diverging cone section and into the absorption section of the vessel. See Figure 2.2.1. One (1) multiple port two fluid nozzle sprays the atomized slurry down the center of the vessel, parallel to the gas glow. The flue gas and the evaporating slurry droplets pass downward toward to the hopper. The flue gas makes a 90° turn and exits the SDA. Ductwork connects the SDA outlet with the

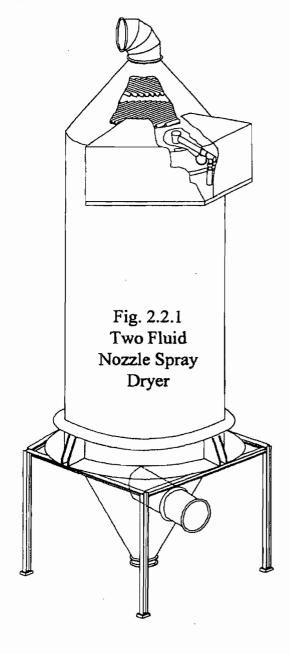
new pulse jet fabric filter (FF) inlet. Some of the flyash from the boiler and dried reaction products fall out of the flue gas and are discharged from the SDA hopper. The down flow design presents several advantages over up flow designs. In a down flow unit, the largest droplets are at a greater distance from the bottom and less likely to hit the sides as gravity affects the flow pattern. In an up flow dryer, drops can hit the walls and dried material can fall on nozzles and disrupt the inlet gas distribution devices.

One (1) 16 ft. diameter SDA is provided for each boiler unit. The SDA is designed to provide 11 seconds flue gas residence time based on the design gas flow conditions (100% MCR).

The top cone of the SDA has two banks of chevrons. Each bank of chevrons is a series of bent plates. The plates help push the gas from the center of the vessel out to chamber walls, resulting in an even distribution of the flue gas across the spray dryer absorber cross section at the slurry injection point.

2.2.1 Atomizing Nozzles

Each SDA will be provided with one (1) operating and one (1) shelf spare nine port two-fluid nozzle. Each two-fluid nozzle consists of a stainless steel (630) head with multiple, ceramic two-fluid nozzle inserts. Each nozzle is provided with a supporting lance assembly



consisting of a structural tube and an aerodynamic shroud (see Figure 2.2.2 and 2.2.3). The lance firmly positions the nozzle in the dryer. The nozzle consists of a 630 SS head with



multiple ceramic inserts. Slurry passes down the enter pipe of the head. The atomizing (compressed) air passes down the annular pipe on the outside of the slurry pipe. Ambient air is induced down the shroud through a silencer (not shown).

Slurry enters the center of the nozzle and is distributed to the back of the inserts (Figure 2.3). Atomizing air passes through the annular space and through the holes in the side of the inserts. The compressed air expands as it passes through these holes and exits the inserts. This expansion accelerates the slurry and shears it into fine droplets. Each nozzle is rated at a maximum flow of 15 gpm.

A minimum of 350 SCFM of compressed air should be supplied to each nozzle.

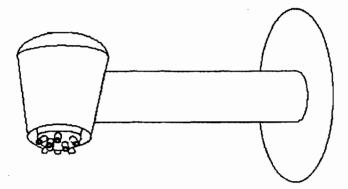


Fig 2.2.2 Multiple Ceramic Insert Single Nozzle w/ Straight Lance

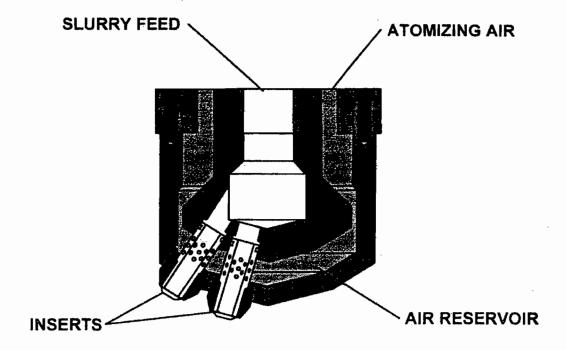
There are three major areas of nozzle maintenance. The most frequent is the external buildup of lime slurry, flyash, or reaction products on the nozzle face. This buildup will grow out from the face around the spray patterns. If it is allowed to grow large enough, it will interfere with the spray pattern, causing the required fine droplets to coalesce into larger ones. This will cause drying and dust discharge problems. A nozzle inspection port is provided to inspect the nozzles the nozzles while the SDA is on-line. This buildup is soft and can be discharged by rapping the back end of the nozzle slurry and air piping with a hammer. Each nozzle should be inspected once a shift by looking in the port to observe buildup and/or poor atomization.



Each nozzle assembly (nozzle, slurry and atomizing air piping) is flanged. Hose connections are provided to connect the nozzle assemblies to the slurry and compressed air manifolds. A nozzle may be isolated, removed, and the spare assembly installed in less than fifteen minutes.

This allows quick change out of spray nozzles for maintenance.

The nozzle inserts are made of a ceramic to minimize erosion. Nozzle wear is monitored



during periodic nozzle inspections. If periodic nozzle inspections are not conducted, nozzle wear can cause a reduction in atomization efficiency. This in turn can cause damp material in the hopper catch and related ash handling problems. Although the ceramic inserts are hard and resistant to wear, they are brittle and easily cracked. Please refer to Section IV of this manual for detailed maintenance procedures for the nozzles.

The minimum orifice size in the nozzles is slightly less than 5/16 inch (7 mm). There is minimal chance of the nozzles plugging. To further minimize this, there is a rotary filter at the nozzle level to act as a final filter. A single plugged nozzle or nozzle port is not a problem in itself. A problem occurs if too many ports are plugged and too much flow is diverted to the remaining nozzles (ports). Then the air/liquid ratio decreases and poor atomization occurs. This problem can be alleviated by periodically inspecting the nozzle operation in the dryer, as described above, for external buildup.

A final feed strainer is provided to remove tramp materials from the slurry and prevent nozzle

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plugging. The strainer includes a circular screen. Slurry enters the center of the screen and passed outward. A circular brush removes collected particles. These drop to a small holding chamber. The holding chamber is isolated and the collected solids blown down to a drain (SDA sump) based on a local timer. A manual basket strainer is installed in a by pass line around the automatic strainer for maintenance.

2.2.2 Hopper

The flue gas passes to the bottom of the spray dryer absorber and then up and out of the side of the vessel. The outlet duct extends into the center of the SDA. This is to maintain an even gas distribution pattern in the bottom of the SDA vessel. A shed plate is installed over the duct, to minimize dust buildup. The majority of the fly ash entering the spray dryer absorber and the solid reaction products generated by the spray dryer absorber are conveyed with the gas to the downstream particulate collection equipment. The remaining portion falls out in the spray dryer absorber hopper. This two-point discharge (flue gas and solids) provides improved operation safety over a one-point dryer discharge where all solids and flue gas exit at one point. The two-point discharge ensures an open flue gas path from the boiler through the spray dryer absorber into the fabric filter should a major dryer upset occur. The design also minimizes the carryover of any wet droplets or moist particulate that may be created by improper drying during upset conditions.

Due to the caking tendency of both the flyash and reaction products, it is recommended that the hoppers be kept as empty as possible and the ash be discharged continuously. To minimize the buildup of ash in the hoppers, the following features are provided:

- Hopper heaters are provided to keep the hopper walls warm. This minimizes the chance of material caking or sticking to the walls.
- A six (6) ft. diameter live bin bottom with an 18" discharge flange is provided on the SDA bottom to minimize rat holing. The activator is interlocked with the ash removal system.
- Air impactor hammers are provided to vibrate walls. These are manually initiated at a panel located at the hopper level for a preset time period and then automatically shut down. The impactors should only be used for upset conditions. Overuse may damage the hoppers.

2.2.3 Access/Nozzle Enclosure

A nozzle enclosure is provided for nozzle and slurry feed control valve maintenance. The enclosure includes a checkered plate floor, drains, ventilation fans, and air intake louvers. There are cross walls between the enclosures. These also serve as pipe bridges.

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The main control loops for the spray dryer absorber are total slurry feed control, which is designed to maintain the SDA outlet temperature (285 °F recommended) and the control of the mixture of concentrated lime slurry and dilution water, to maintain the required SO₂ emission limits (see WAPC Drawing 04-21-3-110). Experience has shown that HCl is absorbed much more readily than SO₂.

Temperature control is considered primary. The SO₂ compliance requirement is averaged over a larger period. SO₂ removal and heavy metal removal are very temperature dependent. The filter cake built up in the Fabric Filter also provides residual SO₂ and HCl control, without slurry feed to the SDA. Instability in temperature control can cause an upset in the SO₂ control loop.

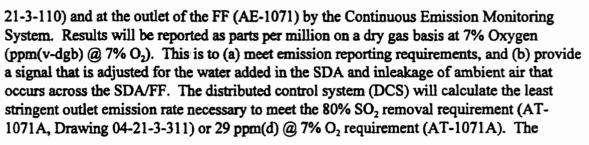
Lime slurry and dilution water are pumped to each SDA. A lime slurry shutoff valve is provided for each SDA (FV-1550). (See drawing No. 04-21-3-110). The lime slurry and dilution water are mixed upstream prior to the SDA Total Feed Control Valve (FCV-1630). This valve is modulated to maintain the flue gas outlet temperature setpoint from the SDA.

Spray dryer inlet, outlet and hopper flue gas temperature will be monitored and recorded at the operator's control console of the DCS. Low outlet temperature (TAL(TIC-1050)) (see Drawing 04-21-3-310) indicates too much slurry is being added to the SDA. This results in damp material in the SD/A hopper catch and related ash handling problems. Alarms are provided for a low and a low-low outlet temperature condition. A low-low condition results in slurry feed shutdown.

The ratio of lime slurry to dilution water is controlled by the SO₂ concentration entering and leaving the system. The spray dryer outlet temperature is monitored by two thermocouples located in the spray dryer outlet ductwork (TE-1050 A&B). Two thermocouples are provided for redundancy. The operator selects which measurement is used for control (HS-1050, Drawing 04-21-3-310). Both measurements are continuously indicated. The selected temperature signal is fed to the spray/dryer outlet temperature controller (TIC-1050), which is used to control the total amount of lime slurry / water mixture entering the SD/A. The output signal from the SDA outlet temperature controller (TIC-1050) is cascaded as a setpoint to the total flow controller (FIC-1551), which adjusts the total flow control valve (FCV-1551) based on a signal from the total flow meter (FIT-1551).

The spray dryer outlet temperature is compared to the spray dryer flue gas temperature measured within the hopper of the SDA (TIT-1100). Operational experiences have shown that if the temperature in the spray dryer hopper is more than 8°F lower than the outlet flue gas temperature, an operation problem is occurring and can typically be traced to poor atomization an/or nozzle problems. An alarm (TDAH-1075) will annunciate this condition and alert the operators to investigate causes and fix the problem.

The concentration of SO₂ will be measured at the inlet of the SDA (AE-1010) (Drawing 04-



DCS will then adjust the ratio of concentrated slurry and dilution water feed to the SD/A to meet the requirement.

The output from the two SO₂ controllers is comparable to the percent dilution water required to maintain SO₂ control. This percent is multiplied by the measured total flow rate to determine the dilution water flow rate. This rate is cascaded as a setpoint to the dilution water flow controller (AIC-1020) which modulates the dilution water flow control valve (FCV-1630) (Drawing - 04-21-3-310) based on a signal from the dilution water flow meter (FY-1630). Dilution water is always controlled at some level below total flow. Lime slurry flow makes up the difference between total and dilution water flow.

A hand control station (HIC-1630) is provided to override the SO₂ controllers during startup or if needed during periods of SO₂ analysis maintenance. This hand controller also includes high and low limits. The low limit is to prevent feeding 100% slurry that has shown to cause nozzle plugging. The high limit is to always assure there is a minimum amount of lime entering the SDA. This is to provide a solid surface to promote drying. There would also be conditions of low SO₂/high HCl concentrations leaving the boiler. This could result, using only SO₂ control in too little lime to control the HCl and a SDA product with high concentrations of calcium chloride (CaCl₂). CaCl₂ is hydroscopic and tends to cake and stick. Providing a minimum lime feed is beneficial for ash handling.

2.3 Absorbent Preparation System

The purpose of the Absorbent Preparation System is to prepare a concentrated lime slurry and dilution water; and pump both streams to the SDA's. The equipment consists of:

- two pebble lime storage silo/accessories
- redundant lime slakers and grit screens
- redundant lime slurry storage tanks
- dilution water tank and grit screen
- redundant lime slurry pump set
- redundant dilution water pumps
- redundant seal water pumps

Process Considerations



a) Slaking System

The primary purpose of the Absorbent Preparation System is to provide a reactive, lime slurry to the SDAs. The slurry consists of very fine calcium hydroxide (Ca(OH)₂) particles suspended in water. The finer the particle, the more SO₂/HCl it will absorb from the flue gas in the SDA.

Pebble lime (sometimes called quick lime) will be supplied in self-unloading trucks and pneumatically conveyed into the storage silo(s). Pebble lime is mostly calcium oxide (approx. 90% by weight). The pebble lime particle size is based on delivery sources will range from granular (<1/8 in.) to pebble size (3/4 in.). Chemically speaking, pebble or quick lime is essentially calcium oxide (CaO). Calcium Oxide is made by heating limestone (calcium carbonate (CaCO₃)) to drive off carbon dioxide molecules from the limestone.

Redundant "paste type" slakers are provided to mix the pebble lime (CaO) with water and produce lime slurry Ca(OH)₂. Chemically, the reaction proceeds as:

$$CaO + H_2O \rightarrow Ca(OH)_2$$

There are three process considerations of which to be aware of when "slaking" lime: (1) the above chemical reaction is "exothermic" which means it releases large amounts of heat. (2) The reaction rate is temperature dependent. The warmer the lime/water mixture is, the faster the reaction progresses, which gives off additional heat. This causes the lime slurry to get hotter, and then gets faster. . . etc. (3) A slurry that is slaked very hot produces a much finer Ca(OH)₂ particle, and a much more reactive slurry. A slurry that is slaked cold, (<170°F) is not as reactive and presents handling problems. Therefore, the lime slakers will also operate very hot (170-212°F). Use caution when working around the slaker, grit screen, slurry tank and pumps.

NOTE: The most important consideration during the lime slaking process is Safety.

Please read the special safety section in this manual relating to the lime system.

The most important consideration during the lime slaking process is Safety. Lime dust (CaO) will react with the moisture on your skin, in you eyes, and in your lungs. It will react with this moisture and create heat causing severe chemical burns. Proper safety equipment must be worn whenever doing maintenance on the silo and lime feeder that meters dry lime into the slaker.

The "paste type" slaker takes advantage of these factors. The paste slaker is a two chamber reactor (See Figure 2.3). The first chamber is similar to a pug mill that mixes the pebble lime and water to make a paste (approximately 40 wt%). The paste



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then is diluted to the design concentration 20 wt% downstream of the paste section. This allows the paste to reach a higher temperature much faster than if a 20 wt% slurry is made in one step because there is less water to heat up.



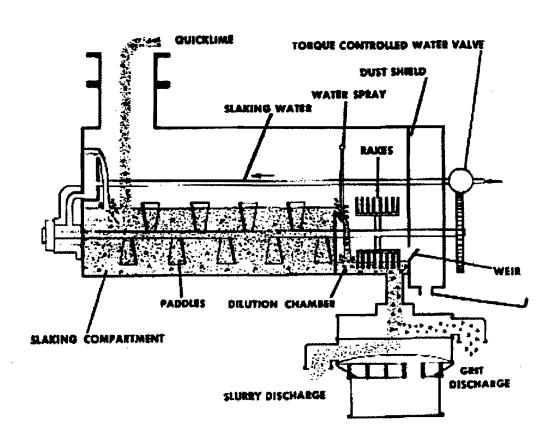


Figure 2.3 Paste Slaker

(b) Dilution Water System

Various sources of water, including plant wastewater, will be used for slurry dilution. The water is considered "hard". Chemically speaking, this means it has a high concentration of liquid phase carbonate (CO₃) and sulfite/sulfate (SO₃/SO₄). When hard water is mixed with lime slurry, a calcium carbonate (CaCO₃) or and/or Calcium Sulfite/Sulfate scale is formed. This would create a severe problem if the hard dilution water was mixed with the lime slurry in the piping immediately upstream of the nozzles. The scale would quickly plug the piping. To slow this type of reaction, a small amount of lime slurry is added in the dilution water tank. This allows many of the scaling reactions to take place within the tank where it is much less of a problem.

2.3.2 Silo

The two lime silos are sized to provide a total of either ten (10) days storage at the MCR Flow/Nominal SO₂/HCl concentration conditions or design (90% UCl) boiler outlet SO₂/HCl

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concentration or 10 days storage (240 hrs) at the average SO₂/HCl concentration with the three boilers operating. Lime will be conveyed from self-loading pneumatic trucks into the silo(s). A limit switch, connected to the fill tube connection, will activate a bin vent filter, located on the silo roof.

High and Low Level alarms are provided for each silo. The high level indicates a full silo and is used to alarm the truck driver not to overfill the silo. The low level indicates that very soon there will be insufficient lime to operate. Level indication is provided on the DCS panel using a sonic type level instrument.

Pebble lime is discharged from each silo using a live bottom through a automatic slide gate type valve to a dedicated slaker. The slide gates are provided for maintenance of the slaker, if required. (See drawing 04-21-3-120.)

2.3.3 Slaking System

Lime is fed from the silo to the slaker using a volumetric screw feeder. The slakers are designed to produce a 22 wt% Ca(OH)₂ slurry (approximately).



Each of the two redundant slaking systems consists of a volumetric feeder, paste slaker, and grit screen. The volumetric feeder is set at a fixed rate based on the slaker capacity and expected lime consumption. Lime falls into the slaker "paste chamber". Water is mixed with the pebble lime using two horizontal paddle agitators. Lime paste overflows a weir at the end of the first chamber and falls into the dilution chamber. An electronic torque valve controls water fed to the first chamber. Electric current to the agitator motor is monitored. Water feed is modulated to maintain a set torque that relates to paste consistency. Water is introduced to the dilution chamber using "cut off" sprays. The spray directs the water to the overflow weir from the paste chamber. This water flow is set manually. The paste chamber agitator blades extend through the dilution chamber. Rakes installed on the shafts mix the paste with the dilution water. The diluted slurry overflows the slaker to the grit screen.

The cut off spray flow rate, as mentioned above, is manually set during start-up. Operation below a critical point will produce too weak of a spray that will not cut the paste as it passes over the weir. This can result in paste plugging the drain line from the slaker to the grit screen. This critical point is close to the maximum flow capacity of the nozzles.

This requires that the slakers be operated over a narrow lime feed rate range. The slakers will be set up to run at approximately 1,200 lbs/hr of pebble lime. Operation above this point will cause too thick a slurry to be made since the dilution spray is set at a fixed flow rate. Operation too far below the set point will cause too thin a slurry to be produced. If the slakers are to operate at a different flow rate, the cut off spray nozzle tips should be changed to match the revised flow rate.

The grit screen is used to remove inert materials and unslaked lime. Slurry flows from each slaker onto a dedicated oscillating grit screen. The oscillating motion causes the collected grits to vibrate toward the discharge chute. The collected grits fall to a grit box at grade. A spray is provided to wash lime from the grit particles. Both grit screens are located above their dedicated lime slurry tank.

The material collected on the grit screen and box should be "clean" sand and gravel particles with a few hard white flakes of hard burned or unreacted quick lime. If there is excessive flakes, it means that the lime slaked was hard burned. If there is excessive white sticky gel, it means that the slaker is not operating properly.

The grit screen has 20 mesh openings. Trace carbon dioxide (CO₂) in the air will react with the lime slurry and cause scale to form on the screen. This will, over several weeks, cause the screen to blind. To remedy this, the screen element is removed and a spare installed. The dirty screen is then soaked in acid to remove the scale. Please refer to the Vendor Slaker Manual.



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2.3.4 Slurry Tanks, Pumps, Recirculation Loop

Lime slurry overflows each slaker grit screen into a dedicated agitated slurry tank. The slurry tanks provide eight (8) hours storage at the design lime consumption rate. Redundant slurry pump sets are provided to pump slurry from the slurry storage tank to the spray dryers and back to the storage tank. Each slurry pump set consists of two slurry pumps in series to produce the necessary head, while maintaining suitable impeller tip speeds. Each slurry pump has a hardened alloy impeller (27% chrome) and a casing liner. The slurry is pumped through single slurry recirculation loop to both SDAs (phase I) and shall flow to all four SDA's upon completion of phase II.

Each pump is provided with a water-flushed packing gland seal. High pressure water is produced by the seal water pumps and is delivered to the packing gland and flows into the slurry feed pumps. Operation without seal water will cause slurry to flow from the pump through the seals and damage the pump shaft and seals and causing messy conditions on the floor. Adequate seal water pressure is a permissive to start the pumps. During operation, low seal water pressure will alarm and stop the pumps.

The lime slurry recirculation loop is utilized to maintain proper flow and pressure to all operating SDA's. Lime slurry consists of suspended particles (approx. 22%) in water. If flow is stopped for an extended time, the particles will settle out, unless the loop is properly flushed and drained. The lime recirculation loop is equipped with automatic flush valves that will open upon pump shutdowns. The recirculation line is flushed back into the slurry storage tank(s) to prevent lime fallout in the pipeline.

2.3.5 Slurry Tank/Recirculation Loop Control

Lime slurry flow in the recirculation loops is controlled to maintain a constant flow leaving the slurry pumps. Slurry flow is measured by a magnetic flow meter (FIT-0520, Drawing 04-21-3-121) and indicated on the DCS. The measured flow is then used to modulate a double pinch valve in the return line to the slurry tank (FCV-0520, Drawing 04-21-3-122). The two (2) valves in series are provided to minimize pressure loss across an individual valve that reduces wear. The valves are a hydraulic type design that compresses around the full circumference. This minimizes wear compared to a mechanical actuator that pinches only from two (2) sides. The two-side pinch produces an internal ridge that erodes faster.

2.3.6 Lime and Water Quality

To produce a reactive lime slurry, a highly reactive pebble or quick lime should be purchased. WAPC recommends that the pebble lime should meet the following requirements:

Size < 3/4"





CAO Content Reactivity per ASTM Slaking Temperature Rise Maximum Reaction Time

minimum 85% < 110-7

4º C / minute 10 minutes

Lower CAO content than specified will effectively lower the capacity rating of the slakers. If a low reactivity lime is supplied, it may not react or slake fully within slaker. This situation will cause the grit screen to plug. Low lime reactivity is a function of the original limestone and how that particular limestone was calcined to make the lime. The lime can be "hard burned". This sinters or produces a hard glassy surface on the lime particles. This slows down the slaking reaction.

Lime samples should be taken periodically and analyzed to assure you are receiving the lime you pay for. It is a good practice to take a sample from every delivery, even if you do not analyze it. The truck driver will see it, and tell the plant, and then you will be less likely to get a bad batch.

This slaking system and lime feeder has been designed to use "pebble lime", or 1/2 or 3/4" particles. Lime is sometimes supplied in granular or powdered form. The slaker will slake granular or powdered lime; however, the lime feeder may flood. This can result in powdered lime flowing through the feeder and out the top of the slaker feed chute creating a severe safety hazard. It is possible to lose a whole silo of lime during these situations.

The "pebble type" design feeder auger has large clearances to prevent binding. The feeder auger may be changed to handle granular or powdered lime, however it must be done prior to receiving this type of lime. The powder design feeder auger or screw, however, will not work with pebble lime.

The primary requirement for water feed to the "paste" chamber is that it contains less than 500 mg/l of total dissolved sulfate, sulfite and bisulfite. These components react with the lime particle or pebble. This prevents the water from reacting with the calcium oxide behind the scale.

2.3.7 Dilution Water

Various sources of water, mainly plant wastewater, is used for slurry dilution. The wastewater is fed to a dilution water tank that holds approximately 2 hours usage (12,000 gal). An oscillating grit screen is provided to filter tramp materials prior to the tank.

Lime slurry is added to the dilution tank to minimize precipitation within the pipelines. This precipitates dissolved carbonates and metals within the wastewater tank, not in the water pipes. If the lime were not added in the tank, the precipitation would occur in the



piping, just upstream of the nozzles, where the dilution water is added to the concentrated lime slurry. The precipitated carbonates would very quickly scale the piping, and restrict the flow.

Two (2) 100% plant capacity pumps are provided to pump water from the dilution water tank to the four SDAs. See Drawing 04-21-3-122. The pumps are arranged in parallel. Both pumps are equipped with manual inlet and outlet isolation valves. A recirculation valve circulates water back to the dilution water tank to maintain a constant flow from the pumps (FCV and FY-0620). This protects the pump from overheating when water demand is low (i.e. one or two SDAs off line).

Water is continuously added to the tank to maintain a preset level. This is accomplished by using a continuous sonic level transmitter (LIT-0600), controller (LIC-0600), and level control valve (LCV-0600). The water flow rate is controlled by tank level. The flow into the tank is monitored (FE-0660).

The pH of the water in the dilution water tank should be monitored periodically. The target pH value is between 11.5 and 12.0. Operating at lower pH values will result in excessive pipe scaling at the nozzle level as solid precipitation will not occur within the tank. Operation above 12.0 pH is also not desirable as scaling potential will not improve much. Higher pH values indicate that too much lime is being added to the tank adding excessive solids to the water system. This will result in premature wear of the dilution water pumps.

2.4 Activated Carbon Injection System

Two Powdered Activated Carbon (PAC) Injection Systems (one for each pair of boilers) are provided to enhance both Mercury and Dioxin/Furan Control. Each system consists of storage silo and three feeder/educator systems (two operating/one spare) to pneumatically feed a controlled amount of PAC into the inlet ductwork of each SDA. The amount of activated carbon feed into the system is manually adjusted. Flow rates will range from 2-25 lbs/hr per boiler. The feeder speed is monitored and recorded by the Continuous Emission Monitor. The initial setpoint is 5 lbs/hr. This will be optimized during start-up.

PAC will be stored in two (2) activated carbon storage silos. One silo is dedicated to one set of boilers. Powdered carbon will be loaded into the silo from pneumatic discharge bulk trucks. Each silo is sized to hold approximately 70,000 lbs of PAC. Each silo will have a multi-pleated bag filter to clean the conveying air from dust.

PAC is discharged through three points in the bottom of the inverted cone hopper. The hopper is fluidized with compressed air to maintain flow. Each discharge point includes a manual slide gate isolation valve. A rotating feeder is used to meter the PAC to a surge hopper/feed chute that supplies PAC to a screw feeder. The screw feeder meters PAC to

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the inlet throat of a venturi educator. A positive displacement blower also feeds air to the back of the venturi. The high air velocity in the venturi throat creates a negative pressure, and sucks in additional air and the PAC. The air expands downstream of the venturi into the piping. Three (3) pipe lines are provided to convey PAC to the SDA inlet ductwork. Flexible hose connections are provided to connect any of the four feeder/eductors to the three conveying lines.

PAC feed from the silo is based on level control in the feed hoppers. See Drawing 04-21-3-128. Upon reaching a low level in one of the hoppers (LSL-0711A) the hopper fluidizing system and rotary valve are started (M-0704A). Feed is stopped when the high level LSH-0710A is reached.

A high and low pressure switches are provided for each conveying line. The high pressure switch indicates a plug and shuts down the feeder in addition to providing an alarm. The low pressure switch (PSH-0723A) alarm indicates a blower or pipeline failure.

Please refer to the Powdered Activated Carbon Injection Manual for more detailed information.

Safety Consideration

Powdered Activated Carbon is very fluid. Proper care must be taken to assure that the silo feed is closed off when doing maintenance on any equipment. Even a small leak can cause the entire content of the silo to empty into the very small equipment enclosure.

It is recommended that the entire feed hopper be emptied before doing any maintenance. This is accomplished by running the feeder and blower in manual with the manual silo knife gate closed.

Pneumatic conveying of PAC also creates static electricity. All equipment should be grounded.

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2.5 Fabric Filter

Each boiler is supplied with a WAPC six (6) module, Size 1211 TA-SB, Model 192 Series 6P Jet III Fabric Filter Pulse-Jet Dust Collector. Each module contains 12 rows of 11 glass fiber bags supported on wire cages.

This system is designed to filter 52,800 acfm of 285°F flyash and hydrated lime dust laden air with a gross air-to-cloth ratio of 2.65:1 (all modules on-line); and a net ratio of 3.18:1 (one (1) module off line); and a net/net ratio of 3.98:1 (two (2) modules off line).

The filter bags for these units are constructed of woven fiber glass with PTFE membrane and acid resistant finish.

These filter bags have the following physical characteristics:

Maximum allowable operating temperature: 525°F

Weight finished 16 oz/sq.yd.

Filter bag diameter 6"
Filter bag length 192"

Modules are 1/4" ASTM A-36, welded, stiffened to withstand ±25" W.G. at 525°F. Hoppers have a minimum valley angle of 60°. Hopper auxiliaries consist of the following:

- 10" x 10" flanged discharge opening
- two (2) 6" x 6" striking anvils
- one (1) 24" diameter hinged access door c/w Viton Seals
- one (1) 20" x 48" hinged plenum access door (oval design)
- one (1) 12" diameter rod out door
- channel frame

One (1) inlet damper is provided for each module. Each damper is a 18" x 36" butterfly type with chain wheel-operated manual actuator. The inlet damper is closed only when a compartment must be isolated for personnel entry when other compartments remain on line.

One (1) outlet damper is provided for each module. Each damper is a 30" diameter poppet type assembly which includes air cylinder, manual lockout, 4-way solenoid valve, air speed control valves, and two (2) limit switches. Outlet dampers must be closed for off-line bag cleaning and isolation for personnel entry when other modules remain on line.

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The Jet III Pulse Jet Fabric Filter Collector is a continuous automatic dust collector capable of filtering dust-laden air through a felted filter media.

The dirty or contaminated gas enters the dust collector through the module inlet. A baffle plate distributes the gas uniformly throughout the housing and drops out the heavy particulate into the hopper. The dust laden air then passes through a number of filter bags which retain the dust particles on the exterior surface while allowing the gas to pass through the module outlet.

As the fabric filter collector operates, the collected dust begins to form a dust cake that eventually diminishes the porosity of the filter bags. This reduction in porosity is measured as pressure loss by the pressure gauges located at each module.

To maintain stable pressure drop a cleaning cycle is employed to provide continuous cleaning of the filter bags. The cleaning system consists of a solid state timer located at each module that actuates electric solenoids governing the air valves. These air valves deliver a momentary burst of pulse of high-pressure compressed air through the manifold pipe into the filter bag. This pulse of air creates a reverse airflow that expands the filter bags to remove the collected dust.

The dust cake, when removed from the filter bag, falls directly into the hopper where it is removed by the dust conveying system.

There is a combination of six (6) possible cleaning formats on the fabric filter collector. The operating mode of the fabric filter collector can be selected to clean either online or offline. Either of the previous states is to be selected and used with one of three (3) cleaning modes. The cleaning modes that control the cleaning operation of the fabric filter collector are: pressure drop (delta-p), time, and manual. The operator may select any one of these three modes depending on the cleaning needs of the fabric filter collector.

It is recommended that the fabric filter collector be cleaned in the online operating mode and the delta-p cleaning mode.

On/off line operating modes

The fabric filter collector will utilize two (2) operating modes of cleaning: online and offline. Online cleaning is done when all of the inlet and outlet dampers of non-isolated modules are open. This will allow all of the modules to be actively filtering while they are cleaning. When using this method of cleaning, the fabric filter collector will clean a predetermined number of filter bags in one module, and then step to the next module in the cleaning sequence. There is a memory built into the cleaning system to ensure that all filter bags are cleaned only once during a cleaning cycle.



The second operating mode of cleaning available is offline cleaning. When a module is cleaned offline, the outlet damper of that module will be closed. With the outlet damper closed, the module is considered to be offline. This operating mode will allow the cleaning of the fabric filter collector one module at a time.

2.5.2 Cleaning Sequence and Pulse Jet Mechanism

The cleaning of the fabric filter system relies on one of three (3) cleaning modes at anytime during the operation. The three modes (manual, time and delta-p) are described below.

2.5.2.1 Manual Cleaning Mode

The manual cleaning mode is primarily to be used as a troubleshooting and maintenance tool. This mode of cleaning will clean one module, on demand, and stop all other automatic cleaning sequences completely. To restart the automatic cleaning, the operator must reset the delta-p or time cleaning mode. The cleaning is done by the operator and is a totally manual procedure. While in manual cleaning, the operator may select any module to be cleaned. The operator action required to initiate this mode of cleaning is as follows:

- select manual cleaning mode.
- 2) select a module to clean. Once the manual mode has been selected the operator may select a module to be cleaned.
- select offline cleaning. When offline cleaning has been selected the operator must manually close the module outlet damper before the module is cleaned.
- 4) start the cleaning cycle. To start the cleaning of the fabric filter, the operator is required to press a start key. When offline cleaning has been selected and the cleaning is complete, the operator must open the module outlet damper.

The operator is to make sure that the system is returned to the delta-p or time mode when finished in the manual cleaning mode.

2.5.2.2 Time Mode

The second mode of cleaning is the <u>time mode</u>. The time mode will clean the fabric filter regardless of the system operating conditions. Cleaning will continue on a strict time basis until the operator changes the cleaning mode.



The operator action required to initiate this mode of cleaning is as follows:

- 1) select online or offline cleaning. The selection of the online or offline mode is to be done as was described earlier.
- 2) select the time cleaning mode. Cleaning will start.

2.5.2.3 Delta-p Mode

The final mode of cleaning the fabric filter is by use of the <u>delta-p mode</u>. When in this mode, the baghouse will clean only when the system differential pressure exceeds the preset value. The differential pressure is measured from the inlet of the fabric filter collector to the outlet of the collector using a differential pressure-indicating transmitter. When a high differential pressure is recognized, the system will clean until the pressure has decreased to an acceptable value. After this has happened, the cleaning cycle will finish cleaning the module selected and then stop its cycle. When the differential pressure again increases to the setpoint, the cleaning cycle will begin again starting with the module following the last one cleaned.

The operator action required to initiate the mode of cleaning is as follows:

- select online or offline cleaning. The selection of the online or offline cleaning mode is to be done as was described earlier.
- 2) select the delta-p cleaning mode.

2.5.2.4 Baghouse Cleaning Timer Adjustment

There are a number of timers needed in order to give the cleaning cycle the versatility needed. The following is a list of timers that will be needed.

- damper close time this timer will allow the outlet damper the correct amount of time needed in order to close. This timer will only be needed in offline method of cleaning.
- 2.) Module clean time this timer will set the amount of time that the Jet III timer boards are to be energized. There will be two timers available to perform this function. There will be one timer for online cleaning and another for offline cleaning. Because of the differences in cleaning methods it may be necessary to clean the modules for different periods of time. The online timer is set to sequential pulse 2-3 rows of bags. The offline timer is set to clean all the bags in a module.



- 3.) settle time - this timer will allow for the dust to settle in the hopper after being cleaned and before the module is brought back into service. If the dust has not settled into the hopper, when the module returns online the dust may be reentrained onto the filter bags. This timer is for offline cleaning only.
- 4.) interval time - this timer will allow the outlet damper to be opened after the module has been cleaned, using the offline mode of cleaning. When using the online mode of cleaning, this timer will act as a transition timer that allows the fabric filter flow to stabilize before cleaning another module whether it be in the online or offline mode.

2.5.2.5 Cleaning Cycle Timer Sequences

The following table indicates the cleaning options and their required timer sequences for the two cleaning methods, online and offline. The cleaning cycle must be programmed using the same sequence of operations as is listed below.

	online	offline
time:	clean time interval time	outlet damper close time clean time settle time interval time
delta-p:	clean time interval time	outlet damper close time clean time settle time interval time
manual:	clean time interval time	outlet damper close time clean time settle time interval time

2.5.2.6 Individual module isolation

The information presented here is to familiarize the fabric filter operators with the recommended procedure for isolating one (1) module from gas flow for personnel entry while the others modules remain on-line filtering.

The following safety rules are recommended for personnel entering an isolated module:

1) Always carry and/or know where the closest communication device is located.



- 2) Any person entering an isolated compartment should be properly attired in coveralls, hard hat, hard soled work shoes and gloves. Also, some form of protective breathing device and eye protection should be used.
- 3) Remove rings, watches, metal frame glasses, etc. Metallic items may be heated by radiation from compartment interior surfaces.
- 4) Never enter an isolated module without having another person standing outside the module door.

2.5.2.7 Module Isolation

Place the selected module isolation switch to the "isolate" position. Tag or lockout switch. The isolation switch is located adjacent to the tubesheet access door. When the isolation switch is turned off, the outlet damper should close, which should be visually verified by the operator. Additionally, the isolation switch locks out the module pulse valves from the control panel so that a module may not be cleaned manually or automatically while it is isolated.

Close the module inlet damper and tag out. The inlet damper is hand operated by pull chain. A padlock placed through the chain links will prevent anyone from opening the inlet damper.

Open the module access door. Allow cool down time before entering the module.

2.5.2.8 Placing module back on-line

After inspection and/or maintenance is complete, the module should be placed back into operation by following this procedure.

- verify that all personnel are out of the compartment.
- close and seal the access door.
- make sure that the hopper door is also closed and sealed.
- remove tag and/or unlock the isolation switch.
- place the isolation switch into "in-service" (outlet damper should open).
- remove tag and/or unlock inlet damper.
- open inlet damper via pull chain.

2.5.2.9 Fabric Filter Protective Interlocks

The following is a summary of abnormal fabric filter operating conditions and the automatic interlocking action that will take place for each. The fabric filter high-high differential pressure will be alarmed at 10" w.c.



The fabric filter low-low inlet temperature will be alarmed at 250°F and a signal is then sent to shutdown the SDA.

The SDA outlet/fabric filter high inlet temperature will be alarmed at 325°F (from TIC-1050).

The fabric filter high-high inlet temperature (TSHH-1050) will be alarmed at 500°F and a signal sent to trip the primary air fan.

2.5.3 Hopper impactor control

Two (2) impactors are provided on each fabric filter compartment hopper to assist in ash removal. Each pair of impactors constitutes a system inasmuch as it is operated in a timed and interlocked sequence.

The hopper impactor system is initiated for a pre-determined time period after one hour of filter operation or when a compartment cleaning cycle is complete. Each time the hopper double dust valve is opened the first impactor (single impact) energizes. After a 5 second delay the second impactor (single impact) energizes. This sequence will continue until the pre-determined time period is complete and the next cleaning cycle is initiated.

Both the impactor "on-time" and maximum interval (one-hour) time can be changed if required to accommodate actual field conditions.

2.5.4 Safety Considerations

- keep alert at all times!
- follow all plant safety regulations concerning protective clothing, eye, ear, and head protection. Always wear your hard hat. Wear safety glasses when working in the absorbent preparation area and when working on the sd/a nozzles on slurry piping. Wear ear protection in the sd/a penthouse.
- follow all caution signs posted throughout the installation. Remember the process uses lime, a caustic chemical.
- study the lockout procedures carefully. Remember the equipment is used to process flue gas which is not safe to breath. Make sure the section you are entering has been ventilated before entering. Only enter the SD/A when the boiler is off. Open the penthouse access door before entering the SD/A hopper. Allow the FF compartments to ventilate for 15 minutes 1 hour before entering. Wear a dust mask when entering any hopper.



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• <u>always</u> make sure a hopper is empty or ash level is below the door level before opening a hopper. Do this by opening a higher level door, or removing a bag from the fabric filter tube sheet. Drowning in hot ash is a terrible way to die.

If there are any questions, contact your supervisor or plant safety personnel. Your safety is your responsibility.



3.0 SNCR NOx Control System

3.1 Process Description

The NOxOUT© Process is a post-combustion NOx reduction method that reduces NOx through a controlled injection of an aqueous solution containing NOxOUT A or other NOxOUT© reagent into the combustion gas path of fossil-fired boilers, furnaces, incinerators or heaters. The reagent is a 50% urea solution plus a small amount of additives for scale and corrosion control. This reagent is readily available and requires no special safety precautions for handling.

The use of urea for control of oxides of nitrogen was developed under the sponsorship of the Electric Power Research Institute (EPRI) between 1976 and 1981. These investigations provided fundamental thermodynamic and kinetic information of the NOx-urea reaction chemistry and identified some traces of by-products. Though some trace quantities of ammonia and carbon monoxide may form, the quantities of these can often be controlled through application know-how. The predominant reaction is described as:

$$CO(NH_2)_2 + 2NO + 1/2 O_2 \rightarrow 6 2N_2 + CO_2 + 2H_2O$$

Urea + 2 Nitrogen Oxide + ½Oxygen \rightarrow 6 Nitrogen + Carbon Dioxide + 2 Water

The NOx removal efficiency and reagent utilization are related by a variable known as Normalized Stoichiometric Ratio (NSR). This ratio is defined as shown below. Reagent utilization is equal to the NOx reduction divided by NSR.

NSR = Actual Molar Ratio of Reagent to Inlet NOx
Stoichiometric Molar Ratio of Reagent to Inlet NOx

The technology has expanded by developing chemical injection hardware, widening the applicable temperature range, and process control expertise required for commercial applications. The technology's licensing agreement with EPRI, combined with successful inhouse developments, is marketed commercially under the trade name NOxOUT©.

Two key parameters that affect the process performance are flue gas temperature and the reagent distribution. The NOx reducing reaction is temperature sensitive; by-product emissions become significant at lower than the optimum temperature range while chemical utilization and NOx reduction decrease at higher than the optimum temperature range. This optimum range is specific to each application. The reagent needs to be evenly and appropriately distributed within this optimum temperature zone to obtain the best performance.



Chemical injectors developed specifically for the process facilitate the reagent distribution. Utilizing pressurized air, these injectors atomize and direct the reagents into the combustion gas path. The droplet size distribution and spray coverage developed by the injectors promote efficient contact between the reagent and NOx in the flue gas.

The process provides effective boiler load following capabilities. Through the computer modeling, an injection strategy can be developed that makes use of multilevel injection, control of reagent concentration, and droplet size and spray patterns.

Several years of field-testing indicate that the NOxOUT© Process is applicable on various types of units firing many different fuels. The process was successfully proven on units fired with coal, oil, gas, wood, or municipal solid or hazardous waste. These units varied in size and type: package boilers, process heaters, incinerators, circulating or bubbling fluidized beds, waste heat boilers, and utility boilers. Being a post-combustion process, size and type of unit and type of fuel have some, but no major, effect on the process.

There are substantial benefits gained from the application of the NOxOUT© Process compared to first generation NOx control technologies, such as ammonia injection. These benefits are:

- Use of non-toxic, non-hazardous chemicals
- Potentially lower capital cost due to the lack of large system compressors and elimination of anhydrous ammonia storage, handling and safety equipment.
- Lower operating costs resulting primarily from minimizing of gas (steam or compressed air) requirements.
- Inherently more effective control of spray patterns and chemical distribution for better mixing with the use of liquid rather than gas-based reagents, thereby resulting in better chemical utilization.
- Chemical enhancers which can be used to improve control of potential byproduct generation while reducing NOx over an expanded temperature range.

3.2 System Description

A reagent storage and delivery system is incorporated to inject the SNCR reagent solution into the combustion gases of the boiler. The concentrated reagent (50% urea) is delivered by truck and transferred into the chemical Storage Tank.

The chemical Storage Tank is a closed top vertical tank, fabricated of fiberglass reinforced polyester and premium grand vinylester resin. It is designed per ASTM D3299-88. The tank is supplied with a level indicator, thermocouple, manway, vent, internal down pipe, external fill pipe, ladder, hold down and lifting lugs, and necessary connections and isolation valves. Site conditions determine the locations of the connections and isolating valves. Site conditions will also determine the need for heat trace, insulation and seismic qualifications.

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The Circulation Module serves the process in a dual role. While its primary purpose is to supply the concentrated chemical to the Metering Modules, it has a secondary purpose of keeping the chemical at a temperature above 80°F, through constant circulation and, if necessary, a circulation heater. The Module is skid mounted and fully shop tested. It consists of redundant centrifugal pumps, an electric in-line heater, a flowmeter, a duplex strainer, one self-contained control panel, and all associated stainless steel pipe, tubing and valves and instrumentation.

The control panel consists of local controls for the Circulation Module. The heater is controlled by a thermostat and is preset to a temperature of 80°F. When the pump is running, and the temperature falls below the setpoint, the heater will automatically activate. The circulation pump should run at all times. The pressure indicators will show if the system is not running properly. There are temperature and pressure indicators, and a flow meter/indicator for monitoring the correct system operation. The local control panel will also digitally show the tank level and temperature.

The Metering Module is a skid mounted unit used to supply diluted chemical to each Distribution Module. The unit is prepackaged and shop tested and includes a chemical metering pump, turbine pump to supply water pressure boost, an in-line mixer, and a local control panel. At the discharge of the boost pump is a recirculation loop with a pneumatic pressure control valve to control flow and pressures to the injectors. In addition, the module contains all necessary valves, check valves, water strainer, flow transmitters, pressure and flow switches and stainless steel piping/tubing to make it a self-contained metering and pumping system. Redundant pumps with motors are provided.

NOx reduction is a function of the chemical feed rate, which is controlled by varying the speed of the metering pumps through a 4-20 mA signal. Control for the Metering Module is provided at the Local Control Panel or from the plant's DCS. The system will operate in local or remote mode. In the local mode, instrumentation and electrical control is performed at the module. In the remote mode, control is performed from the plant DCS. The module also has a hand/auto mode associated with the metering pump and the water boost pump. When the system is in auto and is turned off, the chemical pump will stop, the chemical valve closes and an automatic water flush occurs. In any mode, the pumps will shutdown for low air pressure, low chemical flow, or low water flow. A low low tank level alarm will shut the metering module down in the auto mode. The flow control for the metering pump also has a local and remote mode. In the remote mode, the metering pump receives a 4-20 mA signal from the DCS which controls the pump motor speed. This controls the chemical feed rate. In the local mode, metering pump control is performed at the local control panel using the digital flow controller. Chemical totalization is provided on the flow indicator.

Mixed chemical is transported from the Metering Module to the Distribution Modules, which channel the mixture to each injector. Each Distribution Module consists of flow meters, balancing valves and regulators which accurately control and display the chemical and atomizing air to each injector. Also contained on these modules are the necessary manual ball valves, gauges and stainless steel tubing required to adequately control the injection

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process.

The injectors consist of an atomizing chamber in which the air and chemical mixture first meet. Liquid is sprayed through small orifices forming a jet. The atomizing air shears this jet forming small droplets. The atomized chemical then flows through the injector tube to the nozzle. The nozzle is specially designed and characterized to meet the appropriate plant conditions. The atomized reagent then enters the boiler and mixes with the boiler flue gas to form nitrogen, carbon dioxide and water. Air is required for cooling at any time the injectors are in operation and not retracted from the boiler. The injectors are equipped with quick disconnects and hydraulic hoses for flexibility and ease of maintenance.

The final addition to the injector is an outer cooling air jacket. This shield is attached to the atomizing chamber. Plant air is fed into the coolant air jacket at a low volume and pressure. The air acts as a coolant for the nozzle and the jacket minimizes direct contact between the corrosive flue gas and the injector. This maximizes the useful life of the nozzle in a hostile environment.

4.0 CONTINUOUS EMISSIONS MONITORING SYSTEM

A Continuous Emission Monitoring System is utilized to measure, record and report the performance of the individual boiler trains and their emission control systems to the local Environmental Authorities. Table 1.3 summarizes the data that will be collected. A dedicated multi-component analyzer will be supplied for the inlet of each SDA and the outlet of each FF. An in situ opacity monitor will be installed at each fabric filter outlet. The analyzers are a "Hot-Wet" extractive design. A representative flue gas sample is extracted, filtered and conveyed by heated sampling lines to the analyzer. The analyzer will also be heated to prevent condensation of the moisture in the sample. The outlet test stations are also equipped with opacity monitors. The analyzers are located in an enclosure along with the Data Acquisition System. SO₂ and NO_x signals are fed back via the DCS to the Dry Scrubbing and SNCR Systems. These signals will be used to adjust lime slurry flow (Dry Scrubbing) and NOxOut Solution (SNCR) feed to maintain compliance.

The CEM System is supplied by Aldora. Please refer to their manual for additional information and operating instructions.

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MAJOR AUXILIARY EQUIPMENT LIST

SPRAY DRYER ABSORBER / FABRIC FILTER AREA 5.1

ITEM (P&ID 4-21-3-xxx)	TOTAL (Operating + Spare)
Spray Dryer Absorber (-110)	1(1+0)
SDA Live Bottom (-110)	1(1+0)
SDA Hopper Impactors (-110)	3(3+0)
SDA Hopper Impactor Solenoids (-110)	3(3+0)
Feed Slurry Final Filter (-110)	1(1+0)
SDA Double Slide Gate (-110)	1(1+0)
Fabric Filter Compt No. 1-1 (-111)	1(1+0)
FF Inlet Damper to Compt No. 1-1 (-111)	1(1+0)
FF Outlet Damper from Compt No. 1-1 (-111)	1(1+0)
FF Hopper Compt No. 1-1 Impactor #1 (-111)	1(1+0)
FF Hopper Compt No. 1-1 Impactor #2 (-111)	1(1+0)
FF Compt No. 1-1 Double Dump Valve (-111)	1(1+0)
FF Compt No. 1-1 Screw Conveyor A (-111/112)	1(1+0)
	Spray Dryer Absorber (-110) SDA Live Bottom (-110) SDA Hopper Impactors (-110) SDA Hopper Impactor Solenoids (-110) Feed Slurry Final Filter (-110) SDA Double Slide Gate (-110) Fabric Filter Compt No. 1-1 (-111) FF Inlet Damper to Compt No. 1-1 (-111) FF Outlet Damper from Compt No. 1-1 (-111) FF Hopper Compt No. 1-1 Impactor #1 (-111) FF Hopper Compt No. 1-1 Impactor #2 (-111) FF Compt No. 1-1 Double Dump Valve (-111)

This equipment in §6.1 is shown for Unit #1. For Units #2, #3, and #4, the unit number (fourth digit) is changed to 2 for Unit #2 and 3 for Unit #3 and 4 for Unit #4. See following example:

Unit #1 04-M-1202

Unit #3 04-M-3202

Unit #2 04-M-2202

Unit #4 04-M-4202

This equipment in 6.1 is shown for FF Compt No. 1-1, but is typical for Compt No. 1-2 thru 1-6. For example:



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	Compt No. 1-1 04-M-12 No. 1-2 04-M-12	228 No. 1-5	04-M-1248 04-M-1258 04-M-1268	
04-M-1120 A	No. 1-3 04-M-12 Unit 1 FF Gather Screw		04-MI-1208	1(1+0)
04-M-1120 B	Unit 1 FF Gather Screw	v Conveyor B (-112)		1(1+0)
04-M-1121 A	Unit 1 FF Gather Screw	v Conv. A Disch. Slide	Gate (-112)	1(1+0)
04-M-1121 B	Unit 1 FF Gather Screw	v Conv. B Disch. Slide	Gate (-112)	1(1+0)
04-M-1110	Unit 1 SDA Drag Conv	reyor (-112)		1(1+0)
04-M-1111	Unit 1 SDA Drag Conv	eyor Disch. Slide Gate	(-112)	1(1+0)
04-M-0130 A	Fly Ash Collecting Cor	ıveyor A (-112)		1(1+0)
04-M-0130 B	Fly Ash Collecting Cor	iveyor B (-112)		1(1+0)
04-F-1080	Unit 1 ID Fan (-113)			1(1+0)
04-C-0900 A,B	Atomizing Air Compre	ssors (-125)		2(1+1)
04-T-0910	Atomizing Air Accumu	ılator (-125)		1(1+0)
04-M-0915 A,B	Instrument Air Dryers ((-125)		2(1+1)
04-M-0950 A,B	Glycol Air Coolers (-12	27)		2(1+1)
04-F-0950 A1-A8	Glycol Cooling Fans (-	127)		8(8+0)
04-F-0950 B1-B8	Glycol Cooling Fans (-	127)		8(8+0)
04-C-0900 A,B	Glycol Air Compressor	s (-127)		2(1+1)
04-T-0950	Glycol Surge Tank (-12			1(1+0)
04-P-0950 A,B	Glycol Circulating Pum	nps (-127)		2(1+1)

5.2 REAGENT PREPARATION AREA

EQUIPMENT		TOTAL
NUMBER	<u>ITEM (P&ID 4-21-3-xxx)</u>	(Operating + Spare)

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04-M-0405	Lime Silo Dust Collector (-120)	1(1+0)
04-T-0400 A,B	Lime Silos (-120)	2(2+0)
04-M-0403 A,B	Lime Silo Live Bottoms (-120)	2(2+0)
04-M-0404 A,B	Lime Feeder Inlet Slide Gates (-120)	2(2+0)
04-M-0401 A,B	Lime Feeders (-120)	2(2+0)
04-F-0400 A,B	Lime Slaker Vapor Extractors (-120)	2(2+0)
04-M-0400 A,B	Lime Slakers (-120)	2(2+0)
04-M-0402 A,B	Lime Slurry Grit Screens (-120)	2(2+0)
04-M-0406	Lime Slurry Grit Screw (-120)	1(1+0)
04-T-0500 A,B	Lime Slurry Storage Tanks (-121)	2(2+0)
04-A-0500 A,B	Lime Slurry Storage Tank Agitators (-121)	2(2+0)
04-P-0500 A1,A2,B1,B2	Lime Slurry Feed Pumps (-121)	4(2+2)
04-T-0600	Dilution Water Tank (-122)	1(1+0)
04-A-0600	Dilution Water Tank Agitator (-122)	1(1+0)
04-P-0600 A,B	Dilution Water Pumps (-122)	2(1+1)
04-P-0820 A,B	Seal Water Pumps (-123)	2(1+1)
5.3 SNCR SYSTEM		
EQUIPMENT NUMBER	ITEM (P&ID 4-21-3-xxx)	TOTAL (Operating + Spare)
04-T-0300	SNCR Storage Tank (-130)	1(1+0)
04-P-0300 A,B	SNCR Circulating Pumps (-130)	2(1+1)



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04-H-0301	SNCR In-line Heater (-130)	1(1+0)
04-P-1320 A,B	Unit #1 SNCR Metering Pumps (-131)	2(1+1)
04-P-1330 A,B	Unit #1 SNCR Dilution Water Booster Pumps (-	131) 2(1+1)
5.4 ACTIVATED CAR	BON PREPARATION AREA	
EQUIPMENT NUMBER	ITEM (P&ID 4-21-3-xxx)	TOTAL (Operating + Spare)
04-M-0702 A	Activated Carbon Silo Dust Collector (-128)	1(1+0)
04-T-0700 A	Activated Carbon Silo (-128)	1(1+0)
04-M-0703 A1,A2,A3	Activated Carbon Silo Slide Gates (-128)	3(2+1)
04-M-0704 A1,A2,A3	Activated Carbon Rotary Valves (-128)	3(2+1)
04-T-0701 A1,A2,A3	Activated Carbon Feed Hoppers (-128)	3(2+1)
04-M-0700 A1,A2,A3	Activated Carbon Feeders (-128)	3(2+1)
04-M-0701 A1,A2,A3	Activated Carbon Eductors (-128)	3(2+1)
04-F-0700 A1,A2,A3	Activated Carbon Blowers (-128)	3(2+1)
09-M-0750	Activated Carbon Air Receiver (-128)	1(1+0)

This equipment in §6.3 is shown for Unit #1. For Units #2, #3, and #4, the unit number (fourth digit) is changed to 2 for Unit #2 and 3 for Unit #3 and 4 for Unit #4. See following example:

Unit #1 04-P-1330 Unit #3 04-P-3330 Unit #2 04-P-2330 Unit #4 04-P-4330

This equipment in §6.4 is shown for SDA Units #1 and #2. For Units #3 and #4, change the letter (A) of the tag/equipment number listed to (B). See following example:

Units #1&2 04-T-0700 A

Units #3&4 04-T-0700 B



PROCEDURES FOR STARTUP AND SHUTDOWN



MCKAY BAY REFUSE-TO-ENERGY FACILITY TITLE V RENEWAL APPLICATION

PROCEDURES FOR STARTUP AND SHUTDOWN

The Cover Page and Table of Contents have been provided in lieu of the complete text of the "Wheelabrator McKay Bay, Inc. – Operating Procedures (OP-2 and OP-5)". The complete text is on file at the Facility and is updated annually.

WHEELABRATOR McKAY BAY, INC.

OPERATING PROCEDURES

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WHEELABRATOR MCKAY BAY, INC. OPERATING PROCEDURES

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MALCOLM PIRNIE

OPERATION AND MAINTENANCE PLAN



MCKAY BAY REFUSE-TO-ENERGY FACILITY TITLE V RENEWAL APPLICATION

OPERATION AND MAINTENANCE PLAN

The Cover Page and Table of Contents have been provided in lieu of the complete text of the "Wheelabrator McKay Bay, Inc. – Plant Operations Manual (Volumes I & II)". The complete Manual is on file at the Facility.

WHEELABRATOR MCKAY BAY, INC. PLANT OPERATIONS MANUAL

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TESTING, RECORD KEEPING AND REPORTING

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COMPLIANCE REPORT



MCKAY BAY REFUSE-TO-ENERGY FACILITY TITLE V RENEWAL APPLICATION

COMPLIANCE REPORT AND PLAN

A copy of the 2004 Statement of Compliance dated February 8, 2005 and a summary of the most recent annual compliance testing is included in this Exhibit 12. Annual compliance testing was performed October 5-8, 2005 by CleanAir Engineering, Inc. The report indicated no instances of noncompliance, so a Compliance Plan is not included.

"



Wheelabrator McKay Bay, Inc.

A Waste Management Company

107 North 34th Street Tampa, Florida 33605 (813) 248-1457 (813) 247-2052 Fax

February 8, 2005

Mr. Sterlin Woodard Hillsborough County Environmental Protection Commission 1410 N. 21st Street Tampa, Florida 33605

RE: Permit No. 0570127-001-AV

Annual Statement of Compliance

Dear Mr. Woodard:

In compliance with the subject permit requirements; we have attached DEP Form No. 62-213.900(7), Statement of Compliance – Title V Source. Additional support documentation is maintained at the Facility and available for your review if necessary.

By copy of this letter, we are sending the Statement to U.S. EPA Region 4.

If you have any questions regarding this information, please call me or Mr. Bill Hooper, Director of Environmental, Health and Safety Compliance.

Sincerely,
Mark P. Schwartz

Mark P. Schwartz Plant Manager

Attachment

cc: U. S. EPA Region 4, Air and EPCRA Enforcement Branch

Nancy McCann





Department of Environmental Protection

Division of Air Resource Management

STATEMENT OF COMPLIANCE - TITLE V SOURCE

	Annual Requirement	□ Transfer of Permit		Permanent Facility Shutdown
	REPO	ORTING PERIOD*		REPORT DEADLINE**
	January 1 through	December 31 of 2004 (year)		March 1, 2005
inclu		nust cover all conditions that were in evere added, deleted, or changed through. F.A.C.		•
Facility	y Owner/Company Name:_	City of Tampa		
Site Na	me: McKay Bay Facility	Facility ID No. <u>0570</u>	127	County: Hillsborough
COMP	LIANCE STATEMENT	(Check only one of the following th	ree opti	ons)
	applicable, the Acid Ra requirements associated	in Part, and there were no reporta	able inc of proc	ne Title V Air Operation Permit and, it idents of deviations from applicabless, fuel burning or emission control dabove.
<u>X</u> B.	applicable, the Acid Rais applicable requirements control equipment, or mo	n Part; however, there were one or associated with malfunctions or brea	more reakdowns period	Title V Air Operation Permit and, is portable incidents of deviations from of process, fuel burning or emission identified above, which were reported nation is included:
	 Date of report previ Description of the in 	ously submitted identifying the incidencident.	ent of de	viation.
	applicable, the Acid Rai reportable incidents of de of process, fuel burning of	in Part, EXCEPT those identified in viations from applicable requirement or emission control equipment, or make the control of	n the p s associ onitorin	e Title V Air Operation Permit and, i ages attached to this report and any ated with malfunctions or breakdown g systems during the reporting period item of noncompliance, the following
	 Emissions unit ident Specific permit cond changed during certification 	lition number (note whether the perm	it condit	ion has been added, deleted, or
	•	equirement of the permit condition.		
		ination of noncompliance (for monito recorded at least every 15 minutes, o		meters, indicate whether monitoring ittent).
	5. Beginning and ending	ng dates of periods of noncompliance.		
	6. Identification of the preventative measure	probable cause of noncompliance and es implemented.	descrip	otion of corrective action or
	7. Dates of any reports	previously submitted identifying this	incident	t of noncompliance.

DEP Form No. 62-213.900(7)

Effective: 6-02-02

2. Description of the incident.

1. Date of report previously submitted identifying the incident of deviation.

For each incident of deviation, as described in paragraph B. above, the following information is included:

STATEMENT OF COMPLIANCE - TITLE V SOURCE

RESPONSIBLE OFFICIAL CERTIFICATION

I, the undersigned, am a responsible official (Title V air permit application or responsible official notification form on file with the Department) of the Title V source for which this document is being

submitted. With respect to all matters other than Acid based on the information and belief formed after reasonal contained in this document are true, accurate, and complete	ble inquiry, that the sta	
Janus Zlam		2/2/05
(Signature of Title V Source Responsible Official)		(Dåte)
Name: Nancy McCann	Title: <u>Urban Environn</u> City of Tamp	nental Coordinator na – Solid Waste Dept
DESIGNATED REPRESENTATIVE CERTIFICA	TION (only applicable	e to Acid Rain source)
I, the undersigned, am authorized to make this submission Acid Rain source or Acid Rain units for which the submit that I have personally examined, and am familiar with, the document and all its attachments. Based on my inquiry of for obtaining the information, I certify that the statement knowledge and belief true, accurate, and complete. I am submitting false statements and information or omitting rethe possibility of fine or imprisonment.	ission is made. I certife statements and inform f those individuals with ents and information at aware that there are s	y under penalty of law nation submitted in this a primary responsibility are to the best of my agnificant penalties for
(Signature of Acid Rain Source Designated Representative))	(Date)
Name:	Title:	

(Note: Attachments, if required, are created by a responsible official or designated representative, as appropriate, and should consist of the information specified and any supporting records. Additional information may also be attached by a responsible official or designated representative when elaboration is required for clarity. This report is to be submitted to both the compliance authority (DEP district or local air program) and the U.S. Environmental Protection Agency(EPA) (U.S. EPA Region 4, Air and EPCRA Enforcement Branch, 61 Forsyth Street, Atlanta GA 30303).}

DEP Form No. 62-213.900(7) Effective: 6-02-02

2

Statement of Compliance Title V Source Permit No. 050127-001-AV 2004

The Facility has reported all incidents of deviations from applicable requirements associated with malfunctions or breakdowns of process, fuel burning, emission control equipment, or monitoring systems during the reporting period to the Florida Department of Environmental Protection and the Hillsborough County Environmental Protection Commission in the following documents:

First Quarter 2004 Quarterly Excess Emissions Report Dated April 26, 2004 Second Quarter 2004 Quarterly Excess Emissions Report Dated July 16, 2004 Third Quarter 2004 Quarterly Excess Emissions Report Dated October 20, 2004 Fourth Quarter 2004 Quarterly Excess Emissions Report Dated January 24, 2005 2004 Annual/semi-annual Report dated July 21, 2004 2004 Annual/semi-annual Report dated January 11, 2005 Stack Test Report dated November 22, 2004

WHEELABRATOR MCKAY BAY, INC. TAMPA, FL

Client Reference No: 1320110 CleanAir Project No: 9816-1

PROJECT OVERVIEW

Table 1-2:

Summary of Units 1 and 2 Test Results Permit Average Average Source Unit 1 Unit 2 Limit¹ Constituent Particulate (mg/dscm @ 7% O₂) 1.0 1.0 27 Particulate (lb/hr) 0.0853 0.0863 2.76 Particulate (lb/MMBtu)² 0.000911 0.000936 0.0230 Visual Emissions (%, by COMS) 0.66 10 1.4 Cadmium (mg/dscm @ 7% O₂) 0.00036 0.00022 0.040 4.10E-01 Cadmium (lb/hr) 3.12E-05 1.84E-05 Cadmium (lb/MMBtu)2 3.21E-07 1.99E-07 3.42E-05 Lead (mg/dscm @ 7% O₂) 0.00077 0.0015 0.44 0.0451 Lead (lb/hr) 0.0000679 0.000122 Lead (lb/MMBtu)2 6.96E-07 3.76E-04 1.31E-06 Mercury (mg/dscm @ 7% O2) or 0.070 0.0038 0.0029 Mercury Removal (%)3,4 93% 97% >85 Hydrogen Chloride (ppmdv @ 7% O2) or 29 4.0 5.2 Hydrogen Chloride Removal (%)3,5 99 99 >95 61.8 ¹⁰ 62.8 ⁹ Max. Demonstrated Combustor Load (Klbs/hr)⁶ NA Max. Demonstrated Particulate Control 315 10 315 ⁹ Device Inlet Temperature (OF) NA Carbon Feed rate (lbs/hr)8 3 NΑ

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¹ Limits obtained from 40 Code of Federal Register part 60 Subpart Cb - Emission Guidelines and Compliance Times for Large Municipal Waste Combustors That Are Constructed on or Before September 20, 1994 published in Federal Register as 62 FR 45123 on December 19, 1995 as modified on August 25, 1997, Florida's Rule 62-296.416, F.A.C. and FDEP Permit 050127-001-AV dated July 19, 2001.

² All lb/MMBtu calculations used Fd of 9,570 for MSW as per Method 19.

³ Removal for mercury and hydrogen chloride calculated in the unit of their standards.

⁴Mercury limit is 0.070 mg/dscm @ 7% O₂ or 85% removal, whichever is less stringent.

 $^{^5\}text{Hydrogen}$ Chloride limit is 29 ppmdv @ 7% O2 or 95% removal, whichever is less stringent.

⁶ From 40CFR60.58b (i) (8) the maximum demonstrated load during PCDDs/PCDFs testing, four hour average.

⁷ From 40CFR60.58b (i) (9) the highest four hour average during PCDDs/PCDFs testing.

⁸ From 40CFR60,58b (m)(1)(i) an average mass carbon rate during mercury testing.

⁹ From CleanAir Cb test report dated November 20, 2003.

¹⁰ From CleanAir Cb test report dated November 19, 2004,

WHEELABRATOR MCKAY BAY, INC. TAMPA, FL

Client Reference No: 1320110 CleanAir Project No: 9816-1

PROJECT OVERVIEW

Table 1-3:

Summary of Units 3 and 4 Test Results				
Source	Average Unit 3	Average Unit 4	Permit Limit ¹	
Constituent				
Particulate (mg/dscm @7% O₂)	1.9	4.8	27	
Particulate (lb/hr)	0.153	0.405	2.76	
Particulate (lb/MMBtu) ²	0.00169	0.00434	0.0230	
Visual Emissions (%, by COMS)	0.82	1.4	10	
Cadmium (mg/dscm @ 7% O₂)	0.00074	0.0016	0.040	
Cadmium (lb/hr)	4.75E-04	1.31E-04	4.10E-01	
Cadmium (lb/MMBtu) ²	6.61E-07	1.48E-06	3.42E-05	
Lead (mg/dscm @ 7% O₂)	0.0062	0.019	0.44	
Lead (lb/hr)	0.000475	0.00154	0.0451	
Lead (lb/MMBtu) ²	5.61E-06	1.75E-05	3.76E-04	
Mercury (mg/dscm @ 7% O₂) or	0.011	0.0045	0.070	
Mercury Removal (%) ^{3, 4}	75%	91%	>85	
Total PCCD/PCDF (ng/dscm @ 7% O₂)	3.1	NA	30	
Total PCCD/PCDF (lb/hr)	2.53E-07	NA	3.07E-06	
Total PCCD/PCDF (lb/MMBtu) ²	2.78E-09	NA	2.56E-08	
Hydrogen Chloride (ppmdv @ 7% O₂) or	6.2	6.7	29	
Hydrogen Chloride Removal (%) ^{3, 5}	99	99	>95	
Fluoride (lb/hr)	<0.0057	<0.0060	1.5	
Fluoride (lb/MMBtu) ²	<0.0000639	<0.0000631	0.0125	
Max. Demonstrated Combustor Load (Klbs/hr) ⁶	62.5	61.0 ⁹	NA	
Max. Demonstrated Particulate Control Device Inlet Temperature (⁰ F) ⁷	315	315 ⁹	NA	
Carbon Feed rate (lbs/hr) ⁸	3	3	NA	

¹ Limits obtained from 40 Code of Federal Register part 60 Subpart Cb - Emission Guidelines and Compliance Times for Large Municipal Waste Combustors That Are Constructed on or Before September 20, 1994 published in Federal Register as 62 FR 45123 on December 19, 1995 as modified on August 25, 1997, Florida's Rule 62-296.416, F.A.C. and FDEP Permit 050127-001-AV dated July 19, 2001.

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² Ali lb/MMBtu calculations used Fd of 9,570 for MSW as per Method 19.

³ Removal for mercury and hydrogen chloride calculated in the unit of their standards.

⁴Mercury limit is 0.070 mg/dscm @ 7% O₂ or 85% removal, whichever is less stringent.

⁵Hydrogen Chloride limit is 29 ppmdv @ 7% O₂ or 95% removal, whichever is less stringent.

⁶ From 40CFR60.58b (i) (8) the maximum demonstrated load during PCDDs/PCDFs testing, four hour average.

⁷ From 40CFR60.58b (i) (9) the highest four hour average during PCDDs/PCDFs testing.

⁸ From 40CFR60.58b (m)(1)(i) an average mass carbon rate during mercury testing.

⁹ From CleanAir Cb test report dated November 11, 2002.

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Opacity and Fugitive Emission Test Results					
Source Constituent Ash Handling System ²	Sampling Method	Average Results	Permit Limit ¹		
Fugitive Emissions	EPA M22	0.033 0.067	<5% of observation time (<10 minutes)		
<u>Lime Silo</u> ³					
Visual Emissions	EPA M9	0	5%		
Carbon Silo A ³	•				
Visual Emissions	EPA M9	0	5%		
Carbon Silo B ³					
Visual Emissions	EPA M9	0	5%		

Table 1-4:

Limits obtained from 40 Code of Federal Register part 60 Subpart Cb - Emission Guidelines and Compliance Times for Large Municipal Waste Combustors That Are Constructed on or Before September 20, 1994 published in Federal Register as 62 FR 45123 on December 19, 1995 as modifed on August 25, 1997, Florida's Rule 62-296.416, F.A.C. and FDEP Permit 050127-001-AV dated July 19,

² The Ash Handling System was observed at various locations for a total of 200 minutes.
³ All silos were observed for one hour.



MCKAY BAY REFUSE-TO-ENERGY FACILITY TITLE V RENEWAL APPLICATION

OTHER INFORMATION REQUIRED BY RULE OR STATUTE

As of the submittal date of this document, no other information related to the emissions units addressed in this application was identified as required by applicable air pollution statutes of the State of Florida or rule of the Department of Environmental Protection.