

UNITED STATES ENVIRONMENTAL PROTECTION AGENCY

REGION IV

345 COURTLAND STREET, N.E.

ATLANTA, GEORGIA 30369RECEIVED

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APR - 8 1992

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Clair H. Fancy, P.E., Chief Bureau of Air Regulation Florida Department of Environmental Regulation Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Bureau of Air Regulation

University of Florida Cogeneration Project (PSD-FL-181) RE:

Dear Mr. Fancy:

This is in response to your letter dated January 16, 1992, which requested assistance in determining the amount of creditable reductions of $NO_{\mathbf{x}}$ emissions which are available from the existing central Heat Plant at the above referenced facility. At issue is the proper use of an AP-42 emission factor for gas/oil fired boilers larger than 100 mmBTU/hr heat input capacity.

The applicant requested that FDER use the discretion allowed under F.A.C., Rule 17-2.100(3)(b) to presume that their actual boiler emissions were equal to the allowable emissions which were based on full load operation. EPA's position on this presumption is stated in the preamble to the August 7, 1980, promulgation of federal Prevention of Significant Deterioration (PSD) regulations at 45 FR 52718:

"EPA believes that, in calculating actual emissions, emission allowed under federally enforceable source-specific requirements should be presumed to represent actual emissions levels. Source-specific requirements include permits that specify operating conditions for an individual source, such as PSD permits, state NSR permits issued in accordance with Section 51.18(j) and other Section 51.18 programs, including Appendix 5 (the offset Ruling), and SIP emissions limitations established for individual sources. presumption that federally-enforceable source-specific requirements correctly reflect actual operating conditions should be rejected by EPA or a state, if reliable evidence is available which shows that actual emissions differ from the level established in the SIP or the permit." (emphasis added)

From the operating reports submitted by the applicant, it is clear that the units in question did not operate at their allowable limits on a yearly average. Consequently, we concur with your determination that permitted allowable emissions are not equivalent to actual emissions for this source and that an estimation of actual emissions must be made.

In an ideal scenario, the applicant would have test data for each boiler at various load conditions along with the hours each boiler operated at the corresponding load in each year. This data would allow for the most accurate calculation of actual emissions during the years in question.

Absent having available or obtaining test data for the specific boilers, the next most accurate method for estimating actual emissions would be to utilize an established emission factor along with available fuel use data. The NO_x emission factor for gas fired boilers found in Table 1.4-1 of AP-42 requires the use of an emission factor adjustment (Figure 1.4-1) for reduced loads in boilers with a heat input capacity of greater than 100 mmBTU/hr. The applicant has argued that the emissions factor adjustment for load should only be applied on an instantaneous basis and should not be used where long-term averaging is involved.

As stated in your February 14, 1992, letter to EPA, your staff have "[f]ound data showing that, for natural gas-fired boilers, NO_X emissions are generally reduced by percentages equal to or greater than the percent load reduction." This point is confirmed in the position taken by EPA's Office of Air Quality Planning and Standards in a January 8, 1992, letter from Mr. Ron Ryan to Mr. John Reynolds of your staff. The letter stated that "[t]he load reduction coefficient determined from Figure 1.4-1 of AP-42 should be used in conjunction with the utility boiler factors in Table 1.4-1 to estimate emissions accurately." The letter further states that "[i]f estimates were made for several representative periods and summed, the result would be more accurate than using a single average load for the entire period." Note that at no time is it stated that the load reduction coefficient should be disregarded if a single average load is utilized.

As a result, the methods of estimation of actual emissions in order of their relative accuracy are as follows:

- 1. Stack tests at various loads along with records of hours operated at corresponding loads;
- 2. AP-42 emissions factors (with load reduction coefficient) along with records of hours operated at corresponding loads;
- 3 AP-42 emission factors (with load reduction coefficient) along with a single average load;
- 4. AP-42 emissions factors (without load reduction coefficient) and an assumption that the unit operated at full load.

To date, the applicant has not submitted data corresponding to stack tests or representative periods of load reduction; therefore, options 1 and 2 are not available. Your staff, in a letter to Florida Power dated December 31, 1991, determined that option 3 would provide a more accurate estimation of actual emissions than the option proposed by the applicant (option 4).

Based on the lack of data available from the applicant, the material submitted by your staff, as well as the position taken by OAQPS, we fully support your determination that in this instance, the use of a single average load factor along with corresponding emission factors (and corrections) from AP-42 would constitute representative actual emissions for the purpose of netting.

For reasons of expediency, Florida Power, in their letter to you dated March 5, 1992, has agreed to calculate actual emissions consistent with your determination. We apologize for any inconvenience caused by the delay in our response; however, based on the available information, we are confident that your determination was the correct one for this case.

If you have any questions or comments on this issue, please contact Mr. Gregg Worley of my staff at (404)347-5014.

Sincerely yours,

Jewell A. Harper, Chief Air Enforcement Branch Air, Pesticides and Toxics Management Division

Ron Ryan, OAQPS cc:

Q. Reynolds
Q. Reynolds
Q. Holladay
Q. Kutima, NE Dist
S. Baruch, NE Vist. Branch
C. Shaw, NPS
LHF/13A/PL
K. Kosky, KBN

Department of Environmental Re Routing and Transmit	
To: (Name, Office, Location) 1.	
Mrs. Chris Shower Nes-	
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It should be emphasized that the definition of "actual emissions" found in Rule 17-2.100 (3) F.A.C. specifically allows the use of different time periods than the last two years if it is more representative of normal operation. Indeed, the definition expressly uses the terms "In general" and "representative" in providing guidance in determining actual emission. The subsequent paragraph expressly allows the Department to use different time periods.

State of Florida Department of Environmental Regulation

District Routing Slip

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	Pensacoia	Northwest District	1 10.
	Panama City	Northwest District Branch Office	
	Tallahassee	Northwest District Branch Office	
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	Punta Gorda	Southwest District Branch Office	
	Bartow	Southwest District Satellite Office	
	Orlando	Central District	
	Melbourne	Central District Satellite Office	
1	Jacksonville	Northeast District	
	Gainesville	Northeast District Branch Office	
	Fort Myers	South District	
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	Port St. Lucie	Southeast District Branch Office	
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To: (Name, A+lanta	
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U.S. EPA, Region	
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4.	
Remarks:	
FYI	
FL Power C	orly wood for copen.
P50-FL-	
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From	Date 4 - 4 - 4 - 4
C. H. Fany	Phone 904-488-/344

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\overline{ds}	From Ken Kosky
	CO. KBN
$\overline{)}$	Phone *
9	FBX # 904-331-900

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TEL No.9043324189

7 P.01 File Cary



April 8, 1992

Mr. C. H. Fancy, P.E., Chief Bureau of Air Regulation Florida Department of Environmental Regulation Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Subject:

Alachua County - A.P. UF Cogeneration Project

AC 01-204652 PSO-FL-181

Attention: John Reynolds

Dear John:

Post-It " brand fax transmittal memo 7671 # of pages > 23.

To John Reynolds From Ken Kosky

Co. + DER Co. + BN

Dept. 91012 - 0100 Phone #

Fax # 922 - 6979 Fax # 904 - 331 - 9000

As we discussed yesterday, I have summarized the last five years of fuel usage for the University of Florida's Central Heat Plant. This summary is presented in Table 1 and is based on fuel usage obtained from the Annual Operating Reports (AORs). I have attached the 1991 and 1987 fuel AORs; the 1988-90 AORs have been previously included in the air permit application.

Table 1 presents the total fuel use and the percent difference from the 5-year average. Since the Central Heat Plant is affected by meteorological conditions, a five year average is more appropriate in determining the "representative" fuel use. As can be noticed from Table 1, the natural gas fuel usage (the primary fuel) was quite different for the years 1988 and 1990. The natural gas fuel use in 1988 was 14.4 percent more than the five year average, while the fuel use in 1990 was 14.2 percent less than the five year average. This difference cancelled out in our use of the 1988 through 1990 average as being "representative" of actual emissions. Indeed, the 1988-90 average was less than I percent different than the five year average. Clearly, an average of the last two years (1990-91) and an average of the last three years (1989-91) are not "representative" of fuel use and therefore emissions. The percent difference for these two averaging periods is greater than several percent.

For fuel oil firing (the standby fuel), fuel use varied considerably. However, fuel oil is less important due to its total contribution to heat input. The averaging period presented in the application (i.e., 1988-90) is less than the five year average.

It should be emphasized that the definition of "actual emissions" found in Rule 17-2.100 (3) F.A.C. specifically allows the use of different time periods than the last two years if it is more representative of normal operation. Indeed, the definition expressly uses the terms "In general" and "representative" in providing guidance in determining actual emission. The subsequent paragraph expressly allows the Department to use different time periods.

C.H. Fancy April 8, 1992 Page 2



It is my professional opinion that we should use the 1988-90 period as being "representative" of actual emissions. The basis for this is threefold. First, this is the averaging period for which the application was based when submitted and for which the Department did not object during the first round of completeness questions. Second, I have demonstrated that this averaging period is "representative" of normal fuel usage. Finally, the issue related to using the load correction factor, which centered around this data, was conceded to the Department. In fact, considerable effort was expended in submitting additional information that was based on using the Department's recommended corrections. Therefore, the 1988-90 period should be used by the Department to define "actual emissions".

Please call if you have any questions.

Sincerely, Temored 7. Justy

Kennard F. Kosky, P.E.

President

Scott Osbourn, FPC cc:

W.W. Vierday, FPC

Project File

CHFIBAIPL

Fohn Ruy wolds

Jewell A. Hanger, EPA

KFK/mlb chais shown, NP3
Andy Knigan, NEO

91062A1/8 04/08/92

Table 1. University of Florida Central Heat Plant 5-Year Fuel Use

Period	Natural Gas (10 ³ cf)	α Difference from 5 year Average	Fuel Oil (gal.)	% Difference from 5 year Average
1987	1,153,937	-1.88%	20,606	-172.20%
1988	1,357,653	14.36%	604,546	74.65%
1989	1,175,617	-0,02%	163,729	-51.03%
1990	1,020,301	-14.16%	6,446	-190.87%
1991	1,171,521	-0.37%	584,213	71.69%
88-90 Average	1,184,524	0.74%	258,240	-6.62%
90-91 Average	1,095,911	-7.03%	295,330	6.80%
87-91 Average	1,175,806	0.00%	275,908	0.00%
89-91 Average	1,122,480	-4.64%	251,463	-9.27%

STATE OF FLORIDA DEPARTMENT OF ENVIRONMENTAL REGULATION

NORTHEAST DISTRICT 3428 BILLS ROAD JACKSONVILLE, FLORIDA 32207 904798-4200



BOB MARTINEZ
DOVERNOR

DALE TWACHTMANN
SECRITARY
EFINEST E FREY
DISTRICT MANAGER
GARY L: SMAFFER
ASSISTANI DISTRICT MANAGER

ANNUAL OPERATION REPORT FORM FOR AIR EMISSIONS SOURCES

For each permitted emission point, please submit a separate report for calendar year 19 91 prior to March 1st of the following year.

I	GENERAL INFORMATION	•	
	1. Source Name: NO. 1 Steam Boiler		
	2. Permit Number: <u>A001-57683</u>		
	3. Source Address: University of Florida:	Physical Plant Div.	Bldg. 473
	. Gainesville, FT. 32611		
	. 4. Description of Source: Black steel st	ack, south end of pla	ant
11	ACTUAL OPERATING HOURS: 2,010.20 hrs/day	days/wk	wks/yr
111	RAW MATERIAL INPUT PROCESS WEIGHT: (List and specify applicable units if other than	separately all materi tons/yr)	als put into process
	Raw Material	Input Proc	ess Weight
			tons/yr
			tons/yr
			* * * - / * *
			1
			tons/yr
IV	PRODUCT OUTPUT (Specify applicable units)		
	Steam at 60 nonlbs per hour		

TOTAL FUEL USAGE including standby fue content (e.g., No. 6 oil with 1% 5).	ls. If fuel is oil, specify type and sulfur
82.014 106 cubic feet Natural Gas	10 ³ Kerosene
N/A 10 gallons Dil.	%S tone Coel
10 gallons Propane	tone Carbonaceous
106 Black Liquor Solida	tons Refuse
Other (Specify type and units)	
EMISSION RATE(5) (tons/yr)	·
Particulates S	ulfur Diexide Total Reduced Sulfur
Nitrogen DxideC	arbon HonoxidaFluorida
Hydrocarbon Other (Spec	ify type and unita)
emission factors drawn from AP 42, etc	e.g., use of fuel and materials balance, .)
CERTIFICATION:	
reby certify that the information given ladge.	in this report is correct to the best of my
SIGNATURE OF OWNER OR	TYPED NAME AND TITLE
AUTHORIZED REPRESENTATIVE	
DATE	

ER Form 17-1,202(6)

ffective November 30, 1982

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DEPARTMENT OF ENVIRONMENTAL REGULATION

NORTHEAST DISTRICT

3426 BILLS ROAD JACKSONVILLE, FLORIDA 32207 (904) 39G 6959



BOB GRAHAM GOVERNOR VICTORIA J TSCHINKEL SECHETARY FINEST L HICY INSTRUCT MANAGER

ANNUAL OPERATION REPORT FORM FOR AIR EMISSIONS SOURCES

For each permitted emission point, please submit a separate report for calendar year 1991 prior to March 1st of the following year.

ermit Number: A001-57683			
** J	bucical Plant Div	z. Blda, 473	
ource Address: University of Florida: Pl	Hysical Litable St.		
			_
escription of Source: <u>Black steel stack</u>	second from sout	h end of plant	
OPERATING HOURS: 4,202.09 hrs/day	days/uk	wks/yr	
Raw Material			_
			_t
			_ _t
•			_ t
			_ı
T OUTPUT (Specify applicable units)	· · · · · · · · · · · · · · · · · · ·	e de Mayor de la companya de la comp	• 1
Steam at 60,000 lbs per hour			
Steam at 60,000 ins her nour			
	L OPERATING HOURS: 4,202.09 hrs/day ATERIAL INPUT PROCESS WEIGHT: (List sepanterity applicable units if other than too Raw Material	L OPERATING HOURS: 4,202.09 hrs/day days/wk ATERIAL INPUT PROCESS WEIGHT: (List separately all mater pecify applicable units if other than tons/yr) Raw Material Input Pro	escription of Source: Black steel stack second from south end of plant L OPERATING HOURS: 4,202.09 hrs/day days/wk wks/yr ATERIAL INPUT PROCESS WEIGHT: (List separately all materials put into pecify applicable units if other than tons/yr) Raw Material Input Process Weight

DER Form 17-1.202(6) Effective November 30, 1982

Page 1 of 2

TOTAL FUEL USAGE including standby content (e.g., No. 6 oil with 1% 5)	fuels, If fuel is of	il, specify type and sulfur
173,630 106 cubic feet Natural Gae		_ 10 ³ Kerosens
N/A- 103 gattons 0i1,	*5	tons Cosl
103 Quillons Propane	anners and an expenses and an expenses and	tone Carbonaceous
10 ⁶ Black Liquor Salida		,
Other (Specify type and units)		·
Ferliculates	Sulfur Diaxide	lotal Reduced Sulfu
Nitrogen Oxade	Carbon Honexide	Fluoride
N/A- 103 gattons Oil, %5 tons Cost		
aby certify that the information givenedge.	en in this report is	correct to the heat of my
SIGNATURE OF OWNER OR	TŸI	PED NAME AND TITLE
DATE		•
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Form 17-1,202(a) clive November 30, 1982

Page 2 of 2

AGINOTE TO STATS

DEPARTMENT OF ENVIRONMENTAL REGULATION

NORTHEAST DISTRICT

3426 BILLS ROAD JACKSONVILLE, FLORIDA 32207 (904) 396-8959



BOB GRAHAM GOVERNOR VICTORIA J. TSCHINKEL SECRETARY EINEST E. FREY DISTRICT MANAGER

ANNUAL OPERATION REPORT FORM FOR AIR EMISSIONS SOURCES

For each permitted emission point, please submit a separate report for calendar year 1991 prior to March 1st of the following year.

GENERAL INFORMAT	ion			
1. Source Name:	NO. 3 Steam Boiler			
	r: _A001=57683			
	os: University of Florida, F			
·	Caincsville, FL 32611			
4. Description	of Source:Black.stcol_stack			
ACTUAL OPERATING	BOORS: 5,371.60 hrs/day	days/wk		
RAW MATERIAL INPI	T PROCESS WEIGHT: (List seps cable units if other than ton	rately all mater s/yr)	rials put into	proce
Raw F	aterial	Input Pro	cess Weight	
	<u> </u>			t on
				ton
	-			ton
				ton
				toni
PRODUCT OUTPUT (S	pecify applicable units)		****	*
Steam at 120	,000 lbs per hour			
	,			· _ _
			· · · · · · · · · · · · · · · · · ·	.
				

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Page 1 of 2

	287.180 106 cubic feet Natur	rn) Gae	10 ³ Karosane
	129.151 10 gallona 6		
	103 gallona Propane		Lone Carbonaceous
			Lone Refuse'
	Other (Specify type and unity	s)	<u> </u>
I	EMISSION RATE(S) (tons/yr)		
	Porticulates	Sulfur Dioxide	Total Reduced Sulfur
	Nitrogen Uxide	Carbon Monoxide	Fluoride
I	METHOD OF CALCULATING EMISSIOn emission factors drawn from A	ON RAIES (e.g., use of fue of 42, etc.)	cendix A. The visiable
	MEIHOD DI CALCULATING EMISSIO emission factors drawn from A EPA method 9 was used as do emission is 8.4 percent opac	ON RAIES (e.g., use of fue of 42, etc.)	t and materials balance,
II het	MEIHOD OF EALCULATING EMISSION emission factors drawn from A EPA method 9 was used as do emission is 8.4 percent opace.	on RAIES (e.g., use of fue of 42, etc.) escribed in 40 cfr 60, app city. The highest six-mir	t and meterials belonce, condix A. The visiable nute average was 10.6 percent.
I I	METHOD OF CALCULATING EMISSION omission factors drawn from A EPA method 9 was used as do emission is 8.4 percent opace. CERTIFICATION: eby certify that the informat	on RAIES (e.g., use of fue of 42, etc.) escribed in 40 cfr 60, app city. The highest six-mir	t and meterials belonce, cendix A. The visiable nute average was 10.6 percent.
II het	METHOD OF CALCULATING EMISSION omission factors drawn from A EPA method 9 was used as do emission is 8.4 percent opace. CERTIFICATION: eby certify that the informat	on RATES (e.g., use of fue of 42, etc.) escribed in 40 cfr 60, appeity. The highest six-min	t and materials balance, cendix A. The visiable nute average was 10.6 percent.

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DEPARTMENT OF ENVIRONMENTAL REGULATION

NORTHEAST DISTRICT

3426 BR LS ROAD JACKSONVILLE, FLORIDA 32207 (904) 396 6959



BOR GRAHAM GOVERNOR VICTORIA J. TSCHINKEL SECRETARY ERNEST E FRCY DISTRICT MANAGER

ANNUAL OPERATION REPORT FORM FOR AIR EMISSIONS SOURCES

For each permitted emission point, please submit a separate report for calendar year 1991 prior to Harch 1st of the following year.

1.	Source Name: NO. 4 Steam Boiler		
,	Permit Number: A001-57683		
	Source Address: University of Florida, F	· · - · · · · · · · · · · · · · · · · · · ·	
	Gainesville, FL 32611		
4.	Description of Source: Black steel stack	second from noru	i end of praire
ACTIV	AL OPERATING BOURS: 4,091.30 hrs/day	dava/vk	wks/vr
	MATERIAL INPUT PROCESS WEIGHT: (List meps		
and a	pecify applicable units if other than to:	irately all mater is/yr)	tate par theo pi
	process approved the second se		
	Raw Material		cess Weight
		Input Pro	
	Raw Material	Input Pro	
	Raw Material	Input Pro	
	Raw Material	Input Pro	
	Raw Material	Input Pro	
	Raw Material	Input Pro	
PRODU	Raw Material CT OUTPUT (Specify applicable units)	Input Pro	
PRODU	Raw Material	Input Pro	
PRODU	Raw Material CT OUTPUT (Specify applicable units)	Input Pro	

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	134.723 106 cubic feet Neture	l Gae	10 ³ Kerosene
	71.254 103 yellone 6	011, 1.5 25	tone Coal
	10) gallons Propana		tons Cerbonaceoup
	10 ⁶ Black Liquor Solid	1 ti	tone Refuée
	Other (Specify type and units)	***************************************	·
	ERISSION RATE(S) (tons/yr)		
-	Particulates	Sulfer Dioxide	Total Reduced Sulfur
	Nitrogen Oxide	Carbon Hanakide	Fluoride
	Hydrocarbon Othe METHOD OF CALCULATING EMISSION Semisation factors drawn from AP TUD method 9 was used as descri	r (Specify type and uni RATES (e.g., use of fue 42, etc.) ibed in 40 cfr 60, appo	ta)
	Hydrocarbon Other Rethon of CALCULATING EMISSION Sectors drawn from AP EPA method 9 was used as describinit is 10 percent opacity.	r (Specify type and uni RATES (e.g., use of fue 42, etc.) ibed in 40 cfr 60, appo	ta)
	Hydrocarbon Othe METHOD OF CALCULATING EMISSION Semisation factors drawn from AP TUD method 9 was used as descri	r (Specify type and uni RATES (e.g., use of fue 42, etc.) ibed in 40 cfr 60, appo	ta)
I C	Hydrocarbon Other Rethon of CALCULATING EMISSION Sectors drawn from AP EPA method 9 was used as describinit is 10 percent opacity.	r (Specify type and uni RATES (e.g., use of fue 42, etc.) ibed in 40 cfr 60, appo The highest six-munute	ta)
i C	Hydrocarbon Othe METHOD OF CALCULATING EMISSION Selection factors drawn from AP EPA method 9 was used as describinit is 10 percent opacity. ERTIFICATION: by certify that the information	r (Specify type and uni RATES (e.g., use of fue 42, etc.) ibed in 40 cfr 60, appo The highest six-munute	ta)
i C	Hydrocarbon Othe METHOD OF CALCULATING EMISSION Selection factors drawn from AP EPA method 9 was used as describinit is 10 percent opacity. ERTIFICATION: by certify that the information	r (Specify type and uni RATES (e.g., use of fue 42, etc.) ibed in 40 cfr 60, appo The highest six-munute	ta)
I C	Hydrocarbon Othe METHOD OF CALCULATING EMISSION Selection factors drawn from AP EPA method 9 was used as describinit is 10 percent opacity. ERTIFICATION: by certify that the information	r (Specify type and unit RATES (e.g., use of fue 42, etc.) ibed in 40 efr 60, appe The highest six-minute or given in this report	endix A. The visible emission was 0 percent.

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AGINO, LEONIDA

DEPARTMENT OF ENVIRONMENTAL REGULATION

NORTHEAST DISTRICT

3476 BILLS ROAD JACKSONVILLE, FLORIDA 37207 (904) 396-6959



BOB GRAHAM GOVERNOR VICTORIA J. TSCHINKEL SECHETARY (1872 STEETHEY PUSTRICT MANAGER

ANNUAL OPERATION REPORT FORM FOR AIR EMISSIONS SOURCES

For each permitted emission point, please submit a separate report for calendar year 1991 prior to Harch lat of the following year.

CE	NERAL INFORMATION			
1.	Source Name:	NO. 5 Steam Boiler		
2.	Permit Number:	A001-57683		
3.		University of Florida; P	nysical Plant Div	. Bldq. 473
•		Gainesville, Fr. 32611		
4.		Source: Black steel star		
ACT	TAL OPERATING HO	URS: 5,294 30 hrs/day	days/wk	•
RAW	MATERIAL INPUT	PROCESS WEIGHT: (List sep ble units if other than to	ns/yr)	
	Ray Nat	erial	Input Pro	oceas Weight
	···			ton
				ton
				ten
PRO	DUCT OFFERT (Sne	ify applicable units)		No. 1500
	, (570			
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I METHOD OF CALCULATING EMISSION RATES (b.g., use of fuel and materials balance, amiamion factors drawn from AP 42, etc.)

Hydrocarbon Other (Specify Lype and unita)_____

Nitragen Oxide _____ Carbon Monoxide _____ Fluoride

EPA method 9 wased used a described in 40 cfr 60, appendix A. The visible emission limit is 10 percent opacity. The highest six-minute average was 1.3 percent.

ITE CERTIFICATION:

hereby certify that the information given in this report is correct to the best of my invience.

SIGNATURE OF UNNER OR AUTHORIZED REPRESENTATIVE TYPED NAME AND TITLE

क्ता वर्षक्रम सिर्मिन केला कर पहालक के प्रेरेड कर होते. **वर्षेड होता कि**

DATE

HR Lorm 17-1,207(6)

Thective November 30, 1982

Pago 2 of 2

DEPARTMENT OF ENVIRONMENTAL REGULATION

NORTHEAST DISTRICT

3426 BILLS ROAD JACKSONVILLE, FLORIDA 32267 (804) 396-6959



BOH GRAHAM GOVERNOR VICTORIA J ISCHINKEL SECHETARY ERNLUT E FREY DISTRICT MANAGÉH

ANNUAL OPERATION REPORT FORM FOR AIR EMISSIONS SOURCES

For each permitted emission point, please submit a separate report for calendar year 19 87 prior to March 1st of the following year.

I	GENERAL INFORMATION	
	1. Source Name: No. 1 Steam Boiler	
	2. Permit Number: <u>A001-57683</u>	
	3. Source Address: University of Florida, Physical Plant Division Building 473	
	Gainesville, Florida 32611 4. Description of Source: Black Steel stack south end of plant	
II	ACTUAL OPERATING HOURS: 651 hrs/daydays/wkwks/yr	
III	RAW MATERIAL INPUT PROCESS WEIGHT: (List separately all materials put into proand specify applicable units if other than tons/yr)	cess
	Raw Material Input Process Weight	
		ons/yr
	t	ons/yr
		ons/yr
		ons/yr
		ons/yr
IV	PRODUCT OUTPUT (Specify applicable units)	
	Steam at 60, 000 lbs per hour	
		i

DER Form 17-1.202(6) Effective November 30, 1982

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Page 1 of 2

V	TOTAL FUEL USAGE including standby fuels. If fuel is oil, specify type and sulfur content (e.g., No. 6 oil with 1% 5).
	26.673 106 cubic feet Natural Cos 103 Kerosene
	0 103 gallons #6 0il, 2 \$5 tons Coal
	tons Euthonaceous
	106 Black Liquor Solids tons Refuse
	Other (Specify type and units)
VI	EHISSION RATE(S) (tons/yr)
	Particulates Sulfur Dioxide Total Reduced Sulfu
	Nitrogen Oxide Carbon Monoxide Fluorida
	Hydrocarbon Dther (Specify type and units)
A11	METHOD OF CALCULATING EMISSION RATES (e.g., use of fuel and materials balance, emission factors drawn from AP 42, etc.)
	NOT TESTED
VII1	CERTIFICATION:
l he (now	reby certify that the information given in this report is correct to the best of my ledge.
•	Ken Kisida, Utilities Manager
	SIGNATURE OF OWNER OR TYPED NAME AND TITLE AUTHORIZED REPRESENTATIVE
E	DATE
	F11.16

DEPARTMENT OF ENVIRONMENTAL REGULATION

NORTHEAST DISTRICT

3476 BILLS ROAD JACKSONVILLE, FLORIDA 32207 (904) 396-8959



BOB GRAHAM GOVERNOR VICTORIA L TSCHINKEL SECRETARY FRNEST C FREY DISSTRICT MANAGER

ANNUAL OPERATION REPORT FORM FOR AIR EMISSIONS SOURCES

For each permitted emission point please submit a separate report for calendar year 1987 prior to March 1st of the following year.

I	GENERAL INFORMATION	
	1. Source Name: No. 2 Steam boiler	
	2. Permit Number: A001-57683	
	3. Source Address: <u>University of Florida</u> Gainesville, Florida 32611	Physical Plant Division, Building 473
	4. Description of Source: Black Steel st	ack second from south end of plant
II.	ACTUAL OPERATING HOURS: 2319 hrs/days	days/wk wks/yr
111	RAW MATERIAL INPUT PROCESS WEIGHT: (List and specify applicable units if other than	separately all materials put into process tons/yr)
	Raw Material	Input Process Weight
		tons/yr
IV	PRODUCT OUTPUT (Specify applicable units)	
	Steam at 60,000 lbs per hour	

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٧	TOTAL FU content	EL USAGE inc. (e.g., No. 6	luding sta oil with	mdby f l∦S).	uels.	If fuel	is oil, s	pecify ty	ne pue ed	lfur
	93.48	106 cubic fo	sot Nature	l Cas		-	103	Kerosene		
	0	10 ³ gallons	#6	Dil,		_ % 5	tone	lao3 c		
		10 ³ gallons	Ргорыпе				tone	3 Carbona	ceous	
		106 Black Li	iquor Soli	аb			toni	Refuse		
	Other (S	pecify type i	and units)			 -			· • •	
/1		RATE(S) (to								
	<u> </u>	Particulet	. ೮೪		Sulfur	Dioxide	·	lotal	l Raduced	Sulfur
. 4	<u> :• · · · · · · · · · · · · · · · · · · </u>	Nitrogen (oxide		Carbon	Monexid	ė <u></u>	Fluot	ide	•
		Hydrocarbo	n Oth	er (Spo	cify ty	pe and t	unita)			
11	METHOD OF	CALCULATING	EMISSION In from AP	RATES 42, et	(e.g.,	use of t	fuel and m	aterials	balance,	
		NOT TESTED								
	ing & 100 to 100 to		agail <u>a</u> ste	9.3 A. 1	. Paglist co	···: .·	1000			
I I I	CERTIFICA	TION:			• •		<i>p</i> .			
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•	1)	1	production of the second	اد ویکوردو و در درون درون درون درون درون	14 01		da, Utili	December 200	ane design.	
	Klen	NATURE OF OW	NE D OD		क भागा बर्क	Ken Kisi	da, Utili	ties Mana	ger	
		RIZED REPRES				•	, TYPED N	инс иий і	1188	
~ _	1 10	1000								

DEPARTMENT OF ENVIRONMENTAL REGULATION

NORTHEAST DISTRICT

3426 BILLS ROAD JACKSONVILLE FLORIDA 32707 (904) 396 6959



BOB GRAHAM GOVERNOR VICTORIA J. TSCHINKEL SECHETARY ERHEST I. FREY INSTRUCT MANAGEH

ANNUAL OPERATION REPORT FORM FOR AIR EMISSIONS SOURCES

For each permitted emission point, please submit a separate report for calendar year 1987 prior to March 1st of the following year.

GEN	NERAL INFORMATION	
1.	Source Name: No. 3 Steam Boiler	*** · ·
2.	Permit Number: A001-57683	·
3.		g 473
	Gainesville, Florida 32611	
4.	Description of Source: Black Steel stack center of the plant	
ACT		
RAW and	MATERIAL INPUT PROCESS WEIGHT: (List separately all materials put into	rocess
	Raw Material Input Process Weight	
		_tons/y
PROI	DUCT OUTPUT (Specify applicable units)	
	Steam at 120,000 lbs per hour	
		_
	1. 2. 3. 4. ACT	1. Source Name: No. 3 Steam Boiler 2. Permit Number: A001-57683 3. Source Address: University of Florida, Physical Plant Division, Euilding Gainesville, Florida 32611 4. Description of Source: Black Steel stack center of the plant ACTUAL OPERATING HOURS: 2622 hrs/&X days/wk wks/yr RAW MATERIAL INPUT PROCESS WEIGHT: (List separately all materials put into pand specify applicable units if other than tons/yr) Raw Material Input Process Weight PRODUCT OUTPUT (Specify applicable units)

DER Form 17-1.202(6) Effective November 30, 1982

content (e.g., No. 6 oil w	i standby fuels. If fuel ith 1% 5).	l is oil, specify type and sulfur	
199.013 106 cubic feet Na	tural Gas	10 ³ Kerosene	
16.823 10 ³ gallona #6	0i1,2	tons Cosl	
10 ³ gallons Propa		tone Carbonaceous	
106 Black Liquor	Salide	tona Refuse	
Other (Specify type and un	its)	·····	
I EMISSION RATE(S) (tons/yr			
Particulates	Sulfur Dioxid	Total Reduced Sul	fur
Nitrogen Dxide	Carbon Honoxi	deFluoride	
Hydrocarbon	Other (Specify type and	units)	
II METHOD OF CALCULATING EMISS emission factors drawn from EPA Method 9 was used	as described in 40 CRD 6	SO Appoint to the second second	
emission limit is 20 percent. north of the	ercent opacity. The hig	hest six-minute average was 13.3	
III CERTIFICATION.		and the state of t	
hereby certify that the information	estion of vanish the sap	att is correct to the best of my	
and the second second	3. [2] - 	sida, Utilitdes Manager	
SIGNATURE OF OWNER OR AUTHORIZED REPRESENTATI		TYPED NAME AND TITLE	; (
February 19, 1988		· · · · · · · · · · · · · · ·	
DATE		•	

STATE OF LEGRIDA

DEPARTMENT OF ENVIRONMENTAL REGULATION

NORTHEAST DISTRICT

3426 BILLS ROAD JACKSONVILLE, FLORIDA 32207 (904) 396-6959



BOB GRAHAM GOVERNOR VICTORIA J. TSCHINKEL SECRETARY ERNEST L. FREY LIBERRICT MANAGER

ANNUAL OPERATION REPORT FORM FOR AIR EMISSIONS SOURCES

For each permitted emission point, please submit a separate report for calendar year 1987 prior to March 1st of the following year.

1	GENERAL INFORMATION	
	1. Source Name: No. 4 Steam boiler	<u> </u>
	2. Permit Number: - 'A001-57683.6'	All the second of the second o
	3. Source Address: University of Florid Gainesville, Florida 32611	la, Physical Plant Division, Building 473
	4. Description of Source: Black steel s	tack second from north end of plant
II	ACTUAL OPERATING HOURS: 6265 hrs/XXX	days/wk wks/yr
III	RAW MATERIAL INPUT PROCESS WEIGHT: (List and specify applicable units if other tha	separately all materials put into process
٠. ٠	. Raw Material	Input Process Weight
		tons/yr
ΤΔ	PRODUCT OUTPUT (Specify applicable units)	
	Steam ar 50,000 lbs per hour	

DER Form 17-1.202(6) Effective November 30, 1982

content (e.g., No. 6 oil with 1%	S).
274.886106 cubic feet Natural G	аэ 10 ³ Keroвene
0.272 103 gallons	1,2_ %5 tons Cosl
10 ³ gallons Propane	tons Carbonaceous
106 Black Liquor Solids	tons Refuse
Other (Specify type and units)	,p = = = = = = = = = = = = = = = = = = =
EMISSION RATE(S) (tons/yr)	
Perticulates	Sulfur Dioxide Total Reduced Sulfur
1 1854 88hid Nitrogen Dxide Courte	Cerbon MonoxideFluoride
	(Specify type and unite)
•	IES (e.g., use of fuel and materials balance.
limit is 20 percent opacity. The	in 40 CFR 60, Appendix A. The visible emission highest six-minute average was 5.4 percent.
II CEDIICICATION.	
nereby certify that the information of owledge.	given in this report is correct to the best of my
en e	
	the state of the s
Kentardu	Ken Kisida, Utilities Manager TYPED NAME AND TITLE
AUTHORIZED REPRESENTATIVE	TYPED NAME AND TITLE
February 19, 1988	

· 끝요 : 19번 : 선턴 = 원원 = 원원 = 교육 2 관련

DEPARTMENT OF ENVIRONMENTAL REGULATION

IORTHEAST DISTRICT

3426 BILLS ROAD JACKSONVILLE, FLOHIDA 37207 (904) 396-6959



BOB CHAHAM GOVERNOR VICTORIA J. TSCHINKEL SECHETARY ERNEST I. FREY DISTRICT MANAGER

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ANNUAL OPERATION REPORT FORM FOR AIR EMISSIONS SOURCES

For each permitted emission point, please submit a separate report for calendar year 1987-000 prior to March 1st of the following year.

I	GEN	ERAL INFORMATION	1					
	1.	Source Name: No. 5 Steam boiler						
: -		Permit Number: A001-57683 Source Address: University of Florida, Physical Plant Division, Building 4	 23					
		Cainesville, Florida 32611						
-	4.	Description of Source: Black Steel stack on north end of plant.						
II	ACT	TUAL OPERATING ROURS: 6766 hrs/dex days/wk wks/yr						
III	BA61	MATERIAL INPUT PROCESS WRIGHT: (List separately all materials put into pris specify applicable units if other than tons/yr)	ocess					
		Raw Material Input Process Weight	tons/yr					
			tons/y					
			tons/y					
			tons/y					
			tons/y					
IV	PRO	ODUCT OUTPUT (Specify applicable units)						
	-8	team at 120,000 1bs per hour	-					
			-					
			-					
			-					

TOTAL FUEL USAGE including standby f content (e.g., No. 6 oil with 1% 5).		fuel is	oil, speci	fy type er	id sulfur	
_559,855 106 cubic feet Natural Gas	10 ³ Kerosene					
3.511 10 ³ gallons #6 0il,	2	¥S	tona Co	a]		
10 ³ gallons Propene			tons Ca	rbonaccous	j	
10 ⁶ Black Liquor Solida			tons Re	fuae		
Other (Specify type and units)						
EMISSION RATE(S) (tone/yr)						
Perticulates	Sulfur D	loxide		Intal Rec	fuced Sulfur	
. T. <u>Neb. Bedornittedgenvoride (madisch e</u>	CátBơn No	noxide		Fluoride	-;	
Hydrocerbon Other (Sp	ncify type	and uni	ts)			
I METHOD OF CALCULATING EMISSION RATES emission factors drawn from AP 42, e	(e.g., us		'			
EPA method 9 was used as described i limit is 20 percent opacity; The hi	in 40 CFR Ighest six	60, Apper	ndix A. The was	e visible	emission ent	
II CERTIFICATION:			States to			
hereby certify that the information given by the control of the co	en in this	report.	is correct	to the be	sat of my	
Same of the state		Sec.		•		
	SKM, Salv	Car Co	\$ 1587.55 (4°)		And The	
/cen s/cura	Ke	Ken Kisida, Utilities Manager TYPED NAME AND TITLE				
AUTHORIZED REPRESENTATIVE	TYPED NAME AND TITLE					
February 19, 1988						
DATE						

Department of Environmental Regulation Routing and Transmittal Slip To: (Name, Office, Location) Ms. Jewell A. Hagier U.S. EPA, Ryion IV Remarks: R50-FL-181 FL Power Corp / U. of Fl. Cogen. othis aness World From 4-7-92 C. H. Fany Phone

Interior



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APR 6 1992

Division of Air sources Management

sent us regarding ruct a cogeneration. Heat Plant. The ximately 100 km 0 km south of the reas administered by

e natural gas-fired 1, 2, and 3, and that for the new turbine. are subtracted from project will result , a small increase in volatile organic .ssions.

the proposed emission both the odeling analysis gible impact on the condition requiring d 3 as soon as the soperated in this

manner, we do not anticipate that the University of Florida project will have a significant impact on sensitive air quality-related resources in the Chassahowitzka or Okefenokee Wilderness Areas.

904-448-1344



United States Department of the Interior



FISH AND WILDLIFE SERVICE 75 Spring Street, S.W. Atlanta, Georgia 30303

RECEIVED

April 2, 1992

APR 6 1992

Division of Air Resources Management

Mr. C. H. Fancy Chief, Bureau of Air Regulation Florida Department of Environmental Regulation Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Dear Mr. Fancy:

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We have completed our review of the material that you sent us regarding Florida Power Corporation's (FPC) application to construct a cogeneration facility at the existing University of Florida Central Heat Plant. The University of Florida is located in Gainesville, approximately 100 km northeast of the Chassahowitzka Wilderness Area and 100 km south of the Okefenokee Wilderness Area, both class I air quality areas administered by the Fish and Wildlife Service.

We understand that FPC is proposing to install a single natural gas-fired combustion turbine that will replace existing boilers 1, 2, and 3, and that existing boilers 4 and 5 will only be used as back-up for the new turbine. When the emission reductions from the existing boilers are subtracted from the emission increases from the proposed turbine, the project will result in a significant increase in carbon monoxide emissions, a small increase in emissions of particulate matter, nitrogen oxides, and volatile organic compounds, and a slight decrease in sulfur dioxide emissions.

We were pleased to see that FPC modeled the impact of the proposed emission increases of nitrogen oxides and particulate matter on both the Chassahowitzka and Okefenokee Wilderness Areas. The modeling analysis indicates that the proposed project would have a negligible impact on the class I areas. We recommend that you draft a permit condition requiring FPC to permanently shut down existing boilers 1, 2, and 3 as soon as the new turbine is operational. As long as the facility is operated in this manner, we do not anticipate that the University of Florida project will have a significant impact on sensitive air quality-related resources in the Chassahowitzka or Okefenokee Wilderness Areas.

We appreciate the opportunity to comment on FPC's permit application. If you have any further questions regarding our comments on this project, please contact Tonnie Maniero of our Air Quality office in Denver at 303/969-2071.

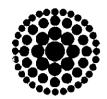
Sincerely yours,

James W. Pulliam, Jr.

Milliaus

Regional Director

CHFIBAIPL Fohn Reynolds
Clone Holladay
Fewell A. Hanger, EPA
Andy Kntyna



Florida Power

RECEIVED

MAR & 1992

Bureau of Air Regulation

March 5, 1992

Mr. C. H. Fancy, P.E., Chief Bureau of Air Regulation Florida Department of Environmental Regulation Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Subject:

Alachua County - A.P. UF Cogeneration Project

AC 01-204652

Dear Clair:

This correspondence provides responses to your letter dated December 31, 1991 as well as revising our application in light the Department's position on the emission factors for load. The responses are presented in the same format as those of your December 31, 1991 letter.

Item 1.

The AP-42 NO_x emission factor for fully loaded natural gas-fired boilers over 100 MMBtu/hr is 550 lbs. NO_x/MM ft³ of fuel fired. For loads less than 100%, the emission factor is reduced according to AP-42, Figure 1.4-1. The 100% factor was used to calculate offset credits of 195.1 tons/yr of NO_x emissions, thus arriving at a net NO_x increase of 38.8 tons/yr. This level of net emissions (less than 40 tons/yr) would preclude PSD review for NO_x as stated in the application. However, analysis of load factors for UF's boilers Nos. 3 and 5 (capacity over 100 MMBtu/hr) during the three period '88 - '90 indicates otherwise.

FPC Response:

The basis of the application has been revised according to the comments made in the Department's December 31, 1991 letter and subsequent correspondence and discussions. Section 2.0 of the PSD permit application has been revised to reflect lower nitrogen oxides (NO_x) emissions from the combustion turbine and duct burner, and further fuel use reductions in Boilers 4 and 5 in the future. These reductions reduce the net emissions increase of NO_x as well as particulate matter and PM10, to below the significant emission rates in Table 500-2 of Rule 17-2 F.A.C. The following is a description of the changes made from the original application.

Mr. C. H. Fancy March 5, 1992 Page 2

Item 1

FPC Response (continued)

a. The capacity factors on the combustion turbine (CT) and duct burner (DB) were reduced. The capacity factor for the CT when firing oil was reduced from 5 percent (438 hours per year at full load) to 2.5 percent (219 hours per year at full load). The capacity factor for firing natural gas in the CT when the maximum oil firing occurs, has been reduced from 95 percent to 93 percent. The application has requested the Department to allow 1.9 hours of natural gas firing for each hour in a given year that oil is not fired at its maximum permitted rate. This would allow up to a 97.75 percent capacity factor for natural gas firing in any year where oil is not fired. The capacity factor for the duct burner has been reduced from 90 percent to 30 percent. Section 2.2 and Tables 2-1 and 2-2 provide a detailed description of the change.

With these revisions, the potential NO_x emissions for the CT/DB are 174.6 tons per year (see Table 2-2). Emissions of other pollutants are also reduced.

b. The NO_x emission factors for Boilers 3 and 5 were revised to be consistent with those calculated by the Department. While we still have technical reservations about using the load correction figure, it is expedient for us to accept the approach based on the needs of the project. It should be recognized by the Department that sufficient information to accurately calculate emissions using this approach does not exist, and previous applications (as well as annual operating reports) did not use this approach.

Tables 2-3 and 2-4 have been revised to reflect the Department's emission factor.

Table 2-5 has been revised to reduce the maximum fuel usage in Boilers 4 and 5. The maximum natural gas and distillate fuel oil usage for Boiler 4 has been reduced from 75 MM ft³/year and 25,000 gallons/year, respectively to 20 MM cf/year and 15,000 gallons/year. Similarly, the fuel use in Boiler 5 has been reduced from 210 MMcf of gas per year and 100,000 gallons of oil per year to 125 MMcf of gas per year and 50,000 gallons of oil per year.

The net NO_x emission reductions from the existing boilers are: 72.2 tons per year from Boilers 1, 2 and 3, and 62.7 tons per year from Boilers 4 and 5 (actual emissions of 82.43 tons per year minus future emissions of 19.73 tons per year). (See Table 2-6 for all net emission reductions.)

Item 2.

References in the application to the proposed facility being major on the basis of emissions exceeding 250 tons per year should be changed to 100 tons per year since the HRSG is on the "List of 28" major source categories (fossil fuel boiler exceeding 250 MMBtu/hr input including GT exhaust).

FPC Response:

The PSD applicability section of the report (i.e., 3.4) has been revised and is attached. The net emissions increase for NO_x is the potential emissions from the project of 174.6 tons per year minus the emission reductions of 134.9 tons per year, or 39.7 tons per year.

Mr. C. H. Fancy March 5, 1992 Page 3

Item 3.

Page 2 of Form 1.202(1), Item C., implies "low NO_x combustors" are being proposed which is not the case. The revised application should explain that Low-NO_x combustors are not currently available for this model turbine but may be within 5 years. The revision should explain what is required in the initial design to provide for future installation of Low-NO_x burners.

FPC Response:

The comment incorrectly assigns meanings to the statements made on page 2 item C of FDER Form 17-1.202(1). The form explicitly uses the language "low NO_x combustors <u>using wet injection</u>". The implication here is that a specially designed combustor using wet injection (i.e., steam) will control NO_x emission. This should not be confused with <u>dry</u> low NO_x combustors which use staged combustion to control NO_x emissions. Dry low NO_x combustors are not available for the aircraft- derivative GE LM 6000 combustion turbine proposed for the project. Inquiries with GE have indicated that a dry low NO_x combustor for this model may be available in mid-1995. Indications are that it may be possible to install this low NO_x combustor on existing machines with a major overhaul. However, the target NO_x emission level is 25 ppmvd corrected to 15 percent oxygen which is the same as that proposed for the project.

Item 4.

Emission calculations are not adequately shown in Appendix A. All calculations affecting emissions should be shown in their entirety. For example, the Appendix "A" calculation for the NSPS NO_x emission limit of 75 ppm corrected to 15 percent oxygen is not carried to completion. The application should clearly show how all emission-related quantities were obtained.

The bases for all calculations are presented in a revised Appendix A. This format has been used and accepted by FDER on previous projects (at least three other projects).

Item 5.

Total steam production should be shown in Table 1-1 along with design capacity of the HRSG.

Total steam production is irrelevant to the air pollutant emissions and NSPS and PSD applicability. Nonetheless, the average steam production when the facility will begin operation in 1994 will be 112,500 lb/hr.

Mr. C. H. Fancy March 5, 1992 Page 4

Item 6.

Please evaluate the impact of this project on the following Class I areas: Chassahowitzka National Wilderness Area in Florida and Okefenokee National Wilderness Area in Georgia. This evaluation should include a cumulative PM₁₀ and NO_x Class I increment analysis. An expanded air quality related values analysis (AQRV) should be done since there are no significant impact levels for this analysis. The AQRV analysis includes impacts to soils, vegetation and wildlife.

Although the proposed permit revision does not trigger PSD review for PM/PM10 and NO_x, the proposed project's PM and NO_x emissions were evaluated at both the Chassahowitzka Wilderness Area (CWA) and the Okefenokee Wilderness Area (OWA). The results for CWA and OWA are summarized in Tables 1 and 2, respectively, for a generic facility emission rate of 10 g/s. The actual PM and NO_x concentrations are compared with suggested Class I significant impact levels (ref: EPA memorandum from John Calcagni dated 9/10/91) for each area in Table 3.

At the CWA, the maximum annual and 24-hour PM concentrations are 0.001 and 0.031 $\mu g/m^3$, respectively. These concentrations are well below the respective Class I significant impact levels of 0.27 and 1.35 $\mu g/m^3$. The maximum NO_x concentration is 0.002 $\mu g/m^3$ which is well below the Class I significant impact level of 0.1 $\mu g/m^3$.

At the OWA, the maximum annual and 24-hour PM concentrations are 0.001 and 0.034 $\mu g/m^3$, respectively. These concentrations are well below the respective Class I significant impact levels of 0.27 and 1.35 $\mu g/m^3$. The maximum NO_x concentration is 0.0025 $\mu g/m^3$ which is well below the Class I significant impact level of 0.1 $\mu g/m^3$.

Based on these analysis, the proposed project is considered to have a negligible impact upon these Class I areas. Therefore, cumulative modeling and AQRV analyses for these areas are not required.

Item 7.

Please explain the use of terrain elevations at receptor points in the modeling and show how the elevations input into the model were derived.

Terrain elevations were included in the impact analysis for the proposed project because the proposed facility's stack height relative to the variation in terrain elevation in the area is not considered large enough to ignore these effects and assume a flat terrain analysis.

The elevations used for the receptors in the modeling analysis were derived from USGS topographical maps of the site vicinity and represent the maximum elevations within a particular screening receptor sector. A receptor's sector includes the area around the receptor up to half the distance to all adjacent receptors, both radially and azimuthally. For the elevations for the furthest receptor ring, the areas to be included beyond that distance are taken to be equal to half the distance between that ring and the next closest ring.

Mr. C. H. Fancy March 5, 1992 Page 5

If you should have any questions or require clarification of the above, please contact Mr. Scott Osbourn of my staff at (813) 866-5158.

Sincerely,

W. Jeffrey Pardue, Manager **Environmental Programs**

Enclosure

cc:

File (2)

bb:\SHO\University of FL Project

CC: J. Reynolds
C. Holladay
G. Kutyna, NE first
J. Berich, NE Dist
G. Harper, EPA
G. Shaver, NPS

Table 1. Maximum Predicted Impacts for the Proposed UF Cogeneration Facility At the Chassahowitzka Wilderness Area Using a Generic Emission Rate of 10 g/s

			Recepto	r Location ^a	
Averaging		Concentration	X	Y	Day/
Time	Year	(μg/m ³)	(m)	(m)	Period
Annual					
	1983	0.007	341100	3183400	- / -
	1984	0.009	341100	3183400	- / -
	1985	0.007	342400	3180600	- / -
	1986	0.007	343700	3178300	- / -
	1987	0.008	341100	3183400	- / -
1-Hour ^b					
	1983	2.366	336500	3183400	159/21
	1984	2.754	341100	3183400	286/ 6
	1985	2.303	334000	3183400	238/23
	1986	2.262	339000	3183400	237/22
	1987	2.961	343700	3178300	199/ 5
3-Hour ^b					
	1983	0.923	342400	3180600	272/ 7
	1984	1.036	339000	3183400	164/ 8
	1985	0.768	334000	3183400	238/ 8
	1986	0.920	336500	3183400	289/ 7
	1987	0.987	343700	3178300	199/ 2
8-Hour ^b					
	1983	0.451	342400	3180600	288/ 1
	1984	0.459	341100	3183400	286/ 1
	1985	0.377	342400	3180600	306/ 3
	1986	0.626	339000	3183400	237/ 3
	1987	0.489	343700	3178300	199/ 1
24-Hourb					
	1983	0.170	342400	3180600	288/ 1
	1984	0.176	341100	3183400	286/ 1
	1985	0.154	343700	3178300	292/ 1
	1986	0.244	339000	3183400	237/ 1
	1987	0.178	343700	3178300	199/ 1

a UTM Coordinates

b All short-term concentrations indicate highest concentrations.

Table 2. Maximum Predicted Impacts for the Proposed UF Cogeneration Facility At the Okefenokee Wilderness Area Using a Generic Emission Rate of $10~\mathrm{g/s}$

			<u>Recepto</u>	r Locationª	
Averaging		Concentration	X	Y	Day/
Time	Year	(μg/m³)	(m)	(m)	Period
Annual					
	1983	0.007	366000	3384000	- / -
	1984	0.008	383000	3382000	- / -
	1985	0.011	380000	3382000	- / -
	1986	0.009	366000	3384000	- / -
	1987	0.008	378000	3382000	- / -
1-Hour ^b					
	1983	2.328	380000	3382000	136/ 3
	1984	2.954	376000	3382000	100/20
	1985	2.349	380000	3382000	192/ 1
	1986	2.344	380000	3382000	267/24
	1987	2.974	366000	3384000	110/22
3-Hour ^b				•	
	1983	1.159	374000	3383000	193/8
	1984	1.278	390000	3410000	187/ 1
	1985	1.361	380000	3382000	233/ 2
•	1986	1.303	366000	3384000	189/8
	1987	1.197	378000	3382000	154/ 2
8-Hour ^b	-	•			•
	1983	0.552	374000	3383000	319/ 1
	1984	0.639	390000	3410000	187/ 1
	1985	0.831	380000	3382000	233/ 1
	1986	0.560	383000	3382000	220/ 1
	1987	0.623	368000	3383000	253/ 1
24-Hourb					
2 . 110 41	1983	0.181	374000	3383000	193/ 1
	1984	0.216	368000	3383000	188/ 1
	1985	0.259	376000	3382000	56/1
	1986	0.206	366000	3384000	189/ 1
	1987	0.267	390000	3384000	354/ 1

a UTM Coordinates

^b All short-term concentrations indicate highest concentrations.

Table 3. Maximum Predicted Pollutant Impacts of the Proposed Facility
Compared to Recommended PSD Class I Significant Impact Levels

Pollutant	Averaging Period	Emission Rate (lb/hr)	Generic Impact (µg/m)	Predicted Impact (µg/m)	Class I Significant Impact Level (µg/m)
<u>CHASSAHOWITZKA</u>	WILDERNESS AR	<u>EA</u>			
Particulate Matter	Annual 24-Hour	10.0	0.009 0.244	0.001 0.031	0.27 1.35
Nitrogen Oxídes	Annual	66.3	0.009	0.007	0.1
OKEFENOKEE WILD	DERNESS AREA				
Particulate Matter	Annual 24-Hour	10.0	0.011 0.267	0.001 0.034	0.27 1.35
Nitrogen Oxides	Annual	66.3	0.011	0.009	0.1

Note: Short-term maximum impacts are highest predicted concentrations for 1983-87.

e:

CERTIFICATION BY A PROFESSIONAL ENGINEER REGISTERED IN FLORIDA

This is to certify that the revisions contained herein have been prepared by me and found to be consistent with my original certification.

Kennard F. Kosky, P.E.

KBN Engineering and Applied Sciences, Inc.

1034 N.W. 57th Street Gainesville, FL 32605

Fla. Registration No. 14996

(904) 331-9000

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SECTION III: AIR POLLUTION SOURCES & CONTROL DEVICES (Other than Incinerators)

A. Raw Materials and Chemicals Used in your Process, if applicable: Not applicable

	Contan	inants	Utilization	Relate to Flow Diagram
Description	Туре	% Wt	Rate - lbs/hr	

1.	Total	Process	Input R	late	(lbs/hr):_	_			
			•		` ' -				

B. Process Rate, if applicable: (See Section V, Item 1) Not applicable

2.	Product Weight	(lbs/hr):	<u>-</u>
	_		

C. Airborne Contaminants Emitted: (Information in this table must be submitted for each emission point, use additional sheets as necessary) See Table 2-1 in PSD Permit application

Name of Contaminant	Emission ¹	Allowed ² Emission Rate per	Allowable ³ Emission	Potential ⁴ Emission		Relate to Flow
	Maximum Actual lbs/hr T/yr	Rule 17-2	lbs/hr	lbs/hr	T/yr	Diagram
SO ₂	197.5 (CT Oil) 13.8	0.8% Sulfur	316.1	197.5	13.8	See
PM	10 (CT Oil) 26.6	NA	NA	10	26.6	Figure 2-1
NO _z	66.3 (CT Oil) 174.6	126 ppuvd	198.9	66.3	174.6	in PSD
со	97.6 (CT DB) 326.7	NA	NA	97.6	326.7	Application
VOC	9.63 (CT DB) 17.5	NA	NA	9.63	17.5	

¹See Section V, Item 2.

²Reference applicable emission standards and units (e.g. Rule 17-2.600(5)(b)2. Table II, E. (1) - 0.1 pounds per million BTU heat input) NSPS--0.8% sulfur oil and 75 ppmvd NO_x corrected for heat rate, i.e., 126 ppmvd; FDER Rule 17-2.660.

³Calculated from operating rate and applicable standard.

⁴Emission, if source operated without control (See Section V, Item 3).

Condition turbine; DB = duct burner Units: Natural GasMMCF/hr; Fuel Oilsgallons/hr; Coal, wood, refuse, otherslbs/h 8.146.8 hr/yr when also firing oil at 219 hours per year; \$2,628 hr/yr; \$219 hr/yr Fuel Analysis: Percent Sulfur: NG = 1 grain/100 CF; oil = 0.5% sulfur Percent Ash: <0.1 Density:7.2 for oil	Name and Type (Model & Serial No.)	Contaminant Eff		(in mic			Basis for Efficiency (Section V Item 5)	
Type (Be Specific) avg/hr								
Type (Be Specific) avg/hr								
Type (Be Specific) avg/hr				<u></u>				
Type (Be Specific) avg/hr								
Type (Be Specific) avg/hr max./hr Maximum Heat Input (MMBTU/hr) Natural Gas-CT 342,071.2 CF2 367,818.5 CF 348 @ Operating Condit Natural Gas-DB 59,302.3 CF2 197,674.4 CF Fuel Oil-CT 1,039.6 lb2 20,792.4 lb 382.6 @ Opera Condit To combustion turbine; DB = duct burner Units: Natural Gas-MMCF/hr; Fuel Oilsgallons/hr; Coal, wood, refuse, otherslbs/h 8,146.8 hr/yr when also firing oil at 219 hours per year; 2,628 hr/yr; 219 hr/yr Percent Sulfur: NG = 1 grain/100 CF; oil = 0.5% sulfur Percent Ash: <0.1 Density: -7.2 for oil leat Capacity: NG = 946 Btu/CF; Oil = 18,400 BTU/lb 132,480 (Oil) Other Fuel Contaminants (which may cause air pollution): See Appendix A in PSD Permit Application F. If applicable, indicate the percent of fuel used for space heating. Annual Average Maximum G. Indicate liquid or solid wastes generated and method of disposal.	. Fuels See Table A-l i							
Natural Gas-CT 342,071.2 CF 367,818.5 CF 348 @ Operating Condit Natural Gas-DB 59,302.3 CF 2 197,674.4 CF Fuel Oil-CT 1,039.6 lbs 20,792.4 lb 382.6 @ Operating Condit T - combustion turbine; DB - duct burner Units: Natural GasMMCF/hr; Fuel Oilsgallons/hr; Coal, wood, refuse, otherslbs/h 8,146.8 hr/yr when also firing oil at 219 hours per year; 2,628 hr/yr; \$219 hr/yr vuel Analysis: ercent Sulfur: NG - 1 grain/100 CF; oil - 0.5% sulfur Percent Ash: <0.1 vensity: -7.2 for oil	Type (Be Specific)							
Fuel Oil-CT 1,039.6 1bs 20,792.4 1b 382.6 @ Operation of turbine; DB = duct burner Units: Natural GasMMCF/hr; Fuel Oilsgallons/hr; Coal, wood, refuse, otherslbs/h 8,146.8 hr/yr when also firing oil at 219 hours per year; 2,628 hr/yr; 219 hr/yr ruel Analysis: Percent Sulfur: NG = 1 grain/100 CF; oil = 0.5% sulfur Percent Ash: <0.1 Pensity: -7.2 for oil Reat Capacity: NG = 946 Btu/CF; Oil = 18,400 BTU/lb 132,480 (Oil) B1 Application F. If applicable, indicate the percent of fuel used for space heating. Annual Average Maximum G. Indicate liquid or solid wastes generated and method of disposal.	Natural Gas-CT		2 CF=		. <u></u>	348 @ Op	erating Condition	
Conditation turbine; DB = duct burner Units: Natural GasMMCF/hr; Fuel Oilsgallons/hr; Coal, wood, refuse, otherslbs/h 8,146.8 hr/yr when also firing oil at 219 hours per year; \$2,628 hr/yr; \$219 hr/yr Fuel Analysis: Percent Sulfur: NG = 1 grain/100 CF; oil = 0.5% sulfur Percent Ash: <0.1 Density: -7.2 for oil lbs/gal Typical Percent Nitrogen: <0.01 Reat Capacity: NG = 946 Btu/CF; Oil = 18,400 BTU/lb 132,480 (Oil) BTU/lb I32,480 (Oil) Other Fuel Contaminants (which may cause air pollution): See Appendix A in PSD Permit Application F. If applicable, indicate the percent of fuel used for space heating. Annual Average Maximum G. Indicate liquid or solid wastes generated and method of disposal.	Natural Gas-DB	59,302.	3 CF ^b	197	,674.4 CF		10	
T = combustion turbine; DB = duct burner Units: Natural GasMMCF/hr; Fuel Oilsgallons/hr; Coal, wood, refuse, otherslbs/h 8,146.8 hr/yr when also firing oil at 219 hours per year; \$2,628 hr/yr; \$219 hr/yr uel Analysis: Percent Sulfur: NG = 1 grain/100 CF; oil = 0.5% sulfur Percent Ash: <0.1 Density:7.2 for oil	Fuel Oil-CT	1,039.	6 1b ^c	20	,792.4 1b		382.6 @ Operation	
Units: Natural GasMMCF/hr; Fuel Oilsgallons/hr; Coal, Wood, Feluse, Otherslos/nr 8,146.8 hr/yr when also firing oil at 219 hours per year; ½2,628 hr/yr; £219 hr/yr Fuel Analysis: Percent Sulfur: NG = 1 grain/100 CF; oil = 0.5% sulfur Percent Ash: <0.1 Pensity: -7.2 for oil lbs/gal Typical Percent Nitrogen: <0.01 Reat Capacity: NG = 946 Btu/CF; Oil = 18,400 BTU/lb 132,480 (Oil) BTU/lb State Contaminants (which may cause air pollution): See Appendix A in PSD Permit Application F. If applicable, indicate the percent of fuel used for space heating. Annual Average Maximum Maxim							Condition	
leat Capacity: NG = 946 Btu/CF; Oil = 18,400 BTU/lb 132,480 (Oil) BTU/lb BTU/lb Application F. If applicable, indicate the percent of fuel used for space heating. Annual Average Maximum	Units: Natural GasMMC 8,146.8 hr/yr when <i>also</i> ^Cuel Analysis:	F/hr; Fuel Oils firing oil at 2	9gal 19 ho	urs per y	year, ~2,0	zo mr/yr, -	21/ 111//1	
Heat Capacity: NG = 946 Btu/CF; Oil = 18,400 BTU/lb 132,480 (Oil) BTU/lb Dther Fuel Contaminants (which may cause air pollution): See Appendix A in PSD Permit Application F. If applicable, indicate the percent of fuel used for space heating. Annual Average Maximum G. Indicate liquid or solid wastes generated and method of disposal.	ercent Sulfur: NG = 1 gr	rain/100 CF; oi	1 - 0.	5% sulfu	<u>r</u> Percent	Ash:_<0.1		
Other Fuel Contaminants (which may cause air pollution): See Appendix A in PSD Permit Application F. If applicable, indicate the percent of fuel used for space heating. Annual Average Maximum G. Indicate liquid or solid wastes generated and method of disposal.	ensity: <u>~7.2 for oil</u>			_ lbs/ga	l Typical	Percent N	itrogen:_ <u><0.015</u> _	
Application F. If applicable, indicate the percent of fuel used for space heating. Annual Average Maximum G. Indicate liquid or solid wastes generated and method of disposal.	leat Capacity: NG = 946 B	:u/CF: 0il = 18	.400	_ BTU/1b	132.48	30 (O11) ·	DED Remit	
F. If applicable, indicate the percent of fuel used for space heating. Annual Average Maximum G. Indicate liquid or solid wastes generated and method of disposal.								
F. If applicable, indicate the percent of fuel used for space heating. Annual Average Maximum G. Indicate liquid or solid wastes generated and method of disposal. All wastewaters generated from the plant will be discharged to the University of Flori	- ·							
G. Indicate liquid or solid wastes generated and method of disposal.	F. If applicable, indica	ate the percent	of fu	iel used	ror space	neacing.		
G. Indicate liquid or solid wastes generated and method of disposar. All wastewaters generated from the plant will be discharged to the University of Floring								
All wastewaters generated from the plant will be discharged to the university of Plot.	G. Indicate liquid or so	olid wastes gen	erated	and met	nou of als	s the Unive	reity of Florida	
wastewater treatment plant.								

2.0 PROJECT DESCRIPTION

2.1 GENERAL DESCRIPTION

The proposed project will consist of installing one CT and one HRSG at the UF Central Heat Plant. The UF Central Heat Plant has five existing boilers which are fired primarily with natural gas; residual oil is used as the backup fuel. The project will replace existing boilers 1, 2, and 3; Boilers 4 and 5 will be operated as backup units for the cogeneration plant. The existing boilers and cogeneration plant will be under the common control of FPC. Therefore, the "facility" for which PSD approval is requested includes the existing Central Heat Plant and the cogeneration plant. This is consistent with the term defined in Florida Department of Environmental Regulation (FDER) Rule 12-2.100(78) Florida Administrative Code (F.A.C.).

The CT will be the new General Electric (GE) LM 6000 machine. The LM 6000 is a newly developed aircraft-derivative machine with a thermal efficiency of approximately 40 percent. This efficiency, developed from advanced aircraft compressor and turbine technology, makes the LM 6000 more efficient than the advanced heavy-frame combustion turbine being offered by certain manufacturers (e.g., the GE Frame combustion turbine). A description of this machine is presented in Appendix A. The CT exhaust will go through the HRSG and exit to the atmosphere through an individual stack. There will be no bypass stack on the CT for simple cycle operation. A flow diagram of the project is presented in Figure 2-1.

The primary fuel for firing the CT will be natural gas; distillate fuel oil will be used as emergency backup when natural gas is curtailed. Operation with distillate oil will not exceed a capacity factor of 2.5 percent or 219 hours per year at full load. There will be supplementary firing of natural gas only in the HRSG.

Air emission sources associated with the proposed project consist of the CT and supplemental firing in the HRSG. Wet injection will be used to control emissions of nitrogen oxides (NO_x) from the CT. The use of natural gas or low-sulfur (0.5-percent-sulfur maximum) distillate fuel oil will minimize the emissions of sulfur dioxide (SO_2) from the unit.

2.2 FACILITY EMISSIONS AND STACK OPERATING PARAMETERS

The emissions and stack parameters for the CT are presented in Table 2-1. These data represent the maximum emissions since air inlet coolers may be installed on the CT to maintain a compressor temperature of 51°F, which will increase generating capability and regulate temperature. Maximum potential annual emissions for the project are presented in Table 2-2. Performance information and maximum emission rates for regulated criteria pollutants, regulated noncriteria pollutants, and nonregulated pollutants from the CT are presented in Tables A-1 through A-5 of Appendix A.

The maximum capacity factors for the combustion turbine will be 93 percent (8,146.8 hours per year) on natural gas and 2.5 percent (219 hours per year) on distillate oil. Because NO_x emissions when firing distillate oil are 1.9 times greater than when firing natural gas, it is requested that the up to 1.9 times more natural gas be allowed for each hour of distillate oil not burned in any given year. The fuel use restriction would be:

Natural Gas Restriction = 348×10^6 Btu/hour x 8,146.8 hours/year = $2,835,086 \times 10^6$ Btu/year and,

Distillate Oil = 382.6×10^6 Btu/hour x 219 hours/year = $83,789 \times 10^6$ Btu/year or,

Natural Gas = 348×10^6 Btu/hr x (8,146.8 + 1.9 x 219 hours/year) = $2.979.889 \times 10^6$ Btu/year or 97.75 percent capacity factor

Supplemental firing with natural gas will take place in the duct between the CT and the HRSG. The supplemental firing, at a maximum rate of 187 million British thermal units per hour (x 10⁶ Btu/hr), will allow the HRSG to produce additional steam. The firing of natural gas will produce additional air emissions, as shown in Tables 2-1 and 2-2, for the maximum firing rate. These emissions will combine with the CT exhaust gases only during natural gas firing and exhaust through the HRSG stack. Supplemental firing will be limited to a 30 percent capacity factor or an equivalent of 2,628 hours per year at maximum capacity (i.e., 491,436 x 10⁶ Btu).

2.3 EXISTING FACILITY EMISSIONS

The proposed facility will include the existing Central Heat Plant which consists of five boilers firing natural gas and residual oil. Boilers 1, 2 and 3 will be taken out of service when the cogeneration plant becomes operational. Boilers 1 and 2 have heat input capacities of 88.5 million Btu per hour. Boiler 3 has a heat input capacity of 160.6 x 10⁶ Btu/hr. Boilers 4 and 5 have heat input capacities of 71.7 and 172.2 x 10⁶ Btu/hr and will be used only as back-up for the cogeneration plant. The primary fuel for these boilers will be natural gas and will be operated at lower capacity factors than in previous years. The use of residual oil in these boilers will be eliminated and replaced with distillate oil. Copies of the FDER permits are contained in Appendix B.

Because the facility consists of the Central Heat Plant, the net emissions decreases are creditable when evaluating PSD applicability [FDER Rule 17-2.500(2)(e)]. For the Central Heat Plant, the actual emissions representative of operation are presented in Table 2-3 for Boilers 1, 2, and 3, and Table 2-4 for Boilers 4 and 5. These emissions represent an average of the last complete 3years (1988-90). A 3-year average is considered representative because operation of the Central Heat Plant is affected by meteorological conditions, i.e. heating and cooling requirements. Three years were used since the calendar year 1990 was abnormally warm compared with historical data. A quantitative measure of this is reflected by the number of heating degree days observed by the National Weather Service for Gainesville. In 1990, the heating degree days were 709 compared to a historical average of 1,259. The average heating degree days for 1990 and 1989 was 974 which would normally be considered the two year period identified in the Department's rules [Rule 17-2.100(3)(a)] as applicable for calculating actual emissions. However, this period was not representative of actual emissions. Therefore, a three year average of 1988 through 1990 was used to calculate actual emissions. The heating degree days for this period is 1,104 which is more representative of the operation of the UF heating plant. Copies of the annual operation reports are contained in Appendix B.

Since Boilers 4 and 5 will be operated as backup units for the cogeneration plant, the operation of these sources will be restricted based on fuel use. The fuel use and emissions are presented in Table 2-5. Also, the emission estimates in this table reflect the use of distillate oil rather than

residual oil. The elimination of Boilers 1, 2, and 3, and the restriction in fuel use and use of distillate oil in Boilers 4 and 5 will provide net emission decreases for the facility which are presented in Table 2-6.

Table 2-1. Stack, Operating, and Emission Data for the UF Cogeneration Facility (Page 1 of 2)

		Fuel Type	
	Fuel Oila	Natura	
Parameter	Gas Turbine	Gas Turbine ^b	Duct Burner ^c
Stack Data (ft)	, ;		
Height	93	93	d
Diameter	9.75	9.75	d
Operating Data			
Temperature (°F)	257	257	d
Velocity (ft/sec)	71.5	72.59	đ
Building Data (ft)			
Height	57	57 -	d
Length	54	54	d
Width	14	14	d
Maximum Hourly Emission Data (II	o/hr) for Each Emission I	Jnit/Fuel Type	
Sulfur Dioxide	197.5	1.05	0.56
Particulate Matter	10.0	2.5	1.87
Nitrogen Oxides	66.3	35.0	18.7
Carbon Monoxide	70.5	69.5	28.1
Volatile Organic Compounds	4.03	1.59	8.04
Sulfuric Acid Mist	15.1	0.08	0.04
Lead	0.0034	Neg	Neg
Annual Potential Emission Data (TI	PY) for Each Emission U	nit/Fuel Type	
Sulfur Dioxide	21.6	4.6	0.74
Particulate Matter	1.1	10.95	2.46
Nitrogen Oxides	7.26	153.4	24.6

e tu

Table 2-1. Stack, Operating, and Emission Data for the UF Cogeneration Facility (Page 2 of 2)

	Fuel Type					
	Fuel Oil ^a	<u>Natura</u>	1 Gas			
Parameter	Gas Turbine	Gas Turbine ^b	Duct Burner ^c			
Carbon Monoxide	7.72	304.4	36.9			
Volatile Organic Compounds	0.44	7.0	10.6			
Sulfuric Acid Mist	1.65	0.3	0.06			
Lead	0.00037	Neg	Neg			

Note: See Tables A-1 through A-5 in the appendix for more detail.

°F = degrees Fahrenheit.

ft = feet.

ft/second = feet per second.

lb/hr = pounds per hour.

TPY = tons per year.

^a Performance based on nitrogen oxide emissions of 42 parts per million by volume dry (corrected to 15 percent O₂); sulfur dioxide emissions based on an average sulfur content of 0.5 percent sulfur; annual emission data based on 2.5 percent capacity factor or 219 hours per year at full load.

b Performance based on nitrogen oxide emissions of 25 parts per million volume dry (corrected to 15 percent O₂); annual emissions data based on 8,760 hours/year (365 days per year) operation.

^c Performance based on 187 x 10⁶ Btu/hr heat input per heat recovery steam generators and 30 percent capacity factor or 2,628 hours per year operation at full load.

d Same as gas turbine natural gas; duct burners will not fire No. 2 oil.

Table 2-2. Maximum Annual Potential Emissions From Proposed Cogeneration Project

	Distillate	Natur	al Gas ^b	Total
Pollutant	Oila	Gas Turbine	Duct Burner	(TPY)
Sulfur Dioxide	21.6	4.3	0.7	26.6
Particulate Matter ^c	1.1	10.2	2.5	13.8
Nitrogen Oxide	7.26	142.7	24.6	174.6
Carbon Monoxide	7.72	282.1	36.9	326.7
Volatile Organic Compounds	0.44	6.5	10.6	17.5
Sulfuric Acid Mist	2.0	0.3	0.05	2.4
Lead	0.00034	Neg	Neg	0.00034

Note: Neg = negative.

PM10 = particulate matter with an aerodynamic diameter less than or equal to 10

micrometers.

TPY = tons per year.

^a219 hours/year.

b93% capacity factor for gas turbine and 30% capacity for duct burner.

^cPM10.

Table 2-3. Actual Representative Emissions (1988-1990) of Regulated Pollutants, Boilers 1, 2, and 3 (Page 1 of 2)

	Boilers 1	No. 1 & 2 ^a	Boile	r No. 3 ^b	
	Natural Gas	No. 6 Fuel Oil	Natural Gas	No. 6 Fuel Oil	Total
Natural Gas Burned ^c					
(MM ft ³ /yr)	208.099		368.275		
No. 6 Fuel Oil ^c					
(gal/yr)		0		12,519	
(% sulfur)		1.85		1.85	
Emission Factor	lb/MM scf	lb/1,000 gal	lb/MM scf	lb/1,000 gal	
Particulate Matter	3	12.64 ^d	3	21.5 ^d	
Particulate Matter (PM10)	3	8.97 ^d	3	15.27 ^d	
Sulfur Dioxide	0.6	151.3 ^e	0.6	290.5°	
Nitrogen Oxides	140	55	310.6 ^f	67	
Carbon Monoxide	35	5	40	5	
Volatile Organic					
Compounds (methane)	3	1	0.3	0.28	
Volatile Organic					
Compounds (nonmethane)	2.8	0.28	1.4	0.76	
Lead	Neg.	0.0042	Neg.	0.0042	
Fluorides	Neg.	0.052	Neg.	0.052	
Mercury	Neg.	0.00048	Neg.	0.00048	
Beryllium	Neg.	0.00063	Neg.	0.00063	
Arsenic	Neg.	0.0029	Neg.	0.0029	
Sulfuric Acid Mist	Neg.	2.32	Neg.	6.57	
Emission Rate (TPY)				-	
Particulate Matter	0.31	0.00	0.55	0.13	1.00
Particulate Matter (PM10)	0.31	0.00	0.55	0.10	0.96
Sulfur Dioxide	0.062	0.00	0.110	1.82	1.99
Nitrogen Oxides	14.57	0.00	57.19	0.42	72.18
Carbon Monixide	3.64	0.00	7.37	0.03	11.04
Volatile Organic					
Compounds (methane)	0.31	0.00	0.06	0.00	0.37

Table 2-3. Actual Representative Emissions (1988-1990) of Regulated Pollutants, Boilers 1, 2, and 3 (Page 2 of 2)

	Boilers No. 1 & 2 ^a		<u>Boiler</u>	Boiler No. 3 ^b	
	Natural Gas	No. 6 Fuel Oil	Natural Gas	No. 6 Fuel Oil	Total
olatile Organic					
Compounds (nonmethane)	0.29	0.00	0.26	0.00	0.55
Lead	Neg.	0.0000	Neg.	0.0000	0.000
Total Fluorides	Neg.	0.000	Neg.	0.000	0.000
Mercury	Neg.	0.00000	Neg.	0.00000	0.000
Beryllium	Neg.	0.00000	Neg.	0.00000	0.00000
Arsenic	Neg.	0.0000	Neg.	0.0000	0.0000
Sulfuric Acid Mist	Neg.	0.00	Neg.	0.04	0.04

Note: Calculations in this table are performed as follows: Fuel use times emission factor equals emission rate; e.g. 208.099 MM scf/yr x 3 lb/MM scf \div 2,000 lb/ton = 0.31 TPY (Note: Roundoff from Lotus may be slightly different than calculations using a calculator.).

 $ft^3/yr = cubic feet per year$

gal/yr = gallons per year

% = percent

lb/mm = pounds per millimeter

scf = standard cubic feet

gal = gallons

Btu/hr = British thermal unit per hour

PM = particulate matte

PM10 = particulate matter (PM10)

TPY = tons per year

^a Boilers 1 and 2 have heat input capacities less than 100 x 10⁶ British thermal units per hour; therefore, emission factors for industrial boilers were used.

b Boiler 3 has a heat input capacity of greater than 100 x 10⁶ British thermal units per hour; therefore, emission factors for utility boilers were used.

^c Based on annual operating reports (see Appendix B).

^d Based on equation: 10 S + 3, where S =sulfur content. PM10 is 71% of PM emissions.

^e Based on equation: 157 S, where S = sulfur content.

f Adjusted based on hours of operation and fuel usage; AP-42 load chart used (see FDER letter of 12/31/91).

Table 2-4. Actual Representative Emissions of Regulated Pollutants, Boilers 4 and 5 (Page 1 of 2)

	Boile	er No. 4 ^a	Boiler	No. 5 ^b	
	Natural	No. 6	Natural	No. 6	 .
	Gas	Fuel Oil	Gas	Fuel Oil	Total
Natural Gas Burned					
(MM ft ³ /yr)	155.542		452.609		
No. 6 Fuel Oil					
(gal/yr)		55,207		190,515	
(% sulfur)		1.623		1.97	
Emission Factor	lb/MM scf	lb/1,000 gal	lb/MM scf	lb/1,000 gal	
Particulate Matter	3	19.23 ^d	3	22.7 ^d	
Particulate Matter (PM10)	3	13.65 ^d	3	16.12 ^d	
Sulfur Dioxide	0.6	254.8 ^e	0.6	309.3°	
Nitrogen Oxides	140	55	281.2 ^f	67	
Carbon Monoxide	35	5	40	5	
Volatile Organic					
Compounds (methane)	3	1	0.3	0.28	
Volatile Organic					
Compounds (nonmethane)	2.8	0.28	1.4	0.76	
Lead	Neg.	0.0042	Neg.	0.0042	
Fluorides	Neg.	0.052	Neg.	0.052	
Mercury	Neg.	0.00048	Neg.	0.00048	
Beryllium	Neg.	0.00063	Neg.	0.00063	
Arsenic	Neg.	0.0029	Neg.	0.0029	
Sulfuric Acid Mist	Neg.	3.98	Neg.	7.0	
Emission Rate (TPY)				-	
Particulate Matter	0.23	0.53	0.68	2.16	3.61
Particulate Matter (PM10)	0.23	0.38	0.68	1.54	2.82
Sulfur Dioxide	0.05	7.03	0.14	29.46	36.68
Nitrogen Oxides	10.89	1.52	63.64	6.38	82.43
Carbon Monoxide	2.72	0.14	9.05	0.48	12.39
Volatile Organic					
Compounds (methane)	0.23	0.03	0.07	0.03	0.36

Table 2-4. Actual Representative Emissions of Regulated Pollutants, Boilers 4 and 5 (Page 2 of 2)

	Boiler No. 4 ^a		Boiler	No. 5 ^b	
	Natural Gas	No. 6 Fuel Oil	Natural Gas	No. 6 Fuel Oil	Total
Volatile Organic					
Compounds (nonmethane)	0.22	0.01	0.32	0.07	0.61
Lead	Neg.	0.0001	Neg.	0.0004	0.0005
Fluorides	Neg.	0.0014	Neg.	0.0050	0.006
Mercury	Neg.	0.00001	Neg.	0.00005	0.00006
Beryllium	Neg.	0.00002	Neg.	0.00006	0.00008
Arsenic	Neg.	0.0001	Neg.	0.0003	0.0004
Sulfuric Acid Mist	Neg.	0.11	Neg.	0.67	0.78

Note: Calculations in this table are performed as follows: Fuel use times emission factor equals emission rate; e.g. $155.542 \text{ MM scf/yr} \times 3 \text{ lb/MM scf} \div 2,000 \text{ lb/ton} = 0.23 \text{ TPY (Note: Roundoff from Lotus may be slightly different than calculations using a calculator.)}$

 $ft^3/yr = cubic feet per year$

gal/yr = gallons per year

% = percent

lb/mm = pounds per millimeter

scf = standard cubic feet

gal = gallons

Btu/hr = British thermal unit per hour

PM = particulate matter

PM10 = particulate matter (PM10)

TPY = tons per year

- ^a Boiler 4 has heat input capacity of less than 100 x 10⁶ Btu/hr; therefore, emissions factors for industrial boilers were used.
- b Boiler 5 has a heat input capacity of greater than 100 x 10⁶ Btu/hr; therefore, emission factors for utility boilers were used.
- ^c Based on annual operating reports (see Appendix B).
- ^d Based on equation: 10 S + 3, where S =sulfur content. PM10 is 71% of PM emissions.
- ^e Based on equation: 157 S, where S = sulfur content.
- f Based on hours of operation and fuel use. Used AP-42 load correction figure (see FDER letter dated 12/31/91).

Table 2-5. Emissions of Regulated Pollutants for Boilers 4 & 5 After Commercial Operation of Cogeneration Plant (Page 1 of 2)

	Boi	ler No. 4ª	E	soiler No. 5 ^b	
	Natural Gas	No. 2 Fuel Oil	Natural Gas	No. 2 Fuel Oil	Total
Natural Gas Burned ^c					
(MM ft ³ /yr)	20		125		
No. 2 Fuel Oil ^e					
(gal/yr)		15,000		50,000	
(% sulfur)		0.5		0.5	
Emission Factor	lb/MM scf	lb/1,000 gal	lb/MM scf	lb/1,000 gal	
Particulate Matter	3	8 _q	3	8 ^d	
Particulate Matter (PM10)	3	5.68 ^d	3	5.68 ^d	
Sulfur Dioxide	0.6	78.5°	0.6	78.5°	
Nitrogen Oxides	140	20	281.2	24	
Carbon Monoxide	35	5	40	5	
Volatile Organic					
Compounds (methane)	3	0.052	0.3	0.052	
Volatile Organic					
Compounds (nonmethane)	2.8	0.2	1.4	0.2	
Lead	Neg.	0.0013	Neg.	0.0042	
Fluorides	Neg.	0.0049	Neg.	0.052	
Mercury	Neg.	0.00045	Neg.	0.00048	
Beryllium	Neg.	0.00038	Neg.	0.00063	
Arsenic	Neg.	0.00063	Neg.	0,0029	
Sulfuric Acid Mist	Neg.	1.225	Neg.	1.225	
Emission Rate (TPY)				-	
Particulate Matter	0.03	0.06	0.19	0.20	0.48
Particulate Matter (PM10)	0.03	0.04	0.19	0.14	0.40
Sulfur Dioxide	0.01	0.59	0.04	1.96	2.59
Nitrogen Oxides	1.40	0.15	17.58	0.61 ^f	19.73
Carbon Monoxide	0.35	0.04	2.50	0.13	3.01
Volatile Organic					
Compounds (methane)	0.03	0.00	0.02	0.00	0.05
Volatile Organic					
Compounds (nonmethane)	0.03	0.00	0.09	0.01	0.12

Table 2-5. Emissions of Regulated Pollutants for Boilers 4 & 5 After Commercial Operation of Cogeneration Plant (Page 2 of 2)

	Boile	r No. 4ª	Boi	ler No. 5 ^b	
	Natural Gas	No. 2 Fuel Oil	Natural Gas	No. 2 Fuel Oil	Total
Y 3	Non	0.00001	Nag	0.00011	0.0001
Lead Fluorides	Neg. Neg.	0.00001	Neg. Neg.	0.0011	0.001
Mercury	Neg.	0.00000	0.0000	0.00001	0.00000
Beryllium	Neg.	0.00000	Neg.	0.00002	0.00002
Arsenic	Neg.	0.00000	Neg.	0.00007	0.0001
Sulfuric Acid Mist	Neg.	0.01	Neg.	0.03	0.04

Note: Calculations in this table are performed as follows: Fuel use times emission factor equals emission rate; e.g. 20 MM scf/yr x 3 lb/MM scf ÷ 2,000 lb/ton = 0.03 TPY (Note: Roundoff from Lotus may slightly different than calculations using a calculator.).

 $ft^3/yr = cubic feet per year$

gal/yr = gallons per year

% = percent

lb/mm = pounds per millimeter

scf = standard cubic feet

gal = gallons

Btu/hr = British thermal unit per hour

PM = particulate matter

PM10 = particulate matter (PM10)

TPY = tons per year

- ^a Boiler 4 has a heat input capacity of less than 100 x 10⁶ Btu/hr; therefore, emissions factors for industrial boilers were used.
- ^b Boiler 5 has a heat input capacity of greater than 100 x 10⁶ Btu/hr; therefore, emission factors for utility boilers were used.
- ^c Based on annual operating reports (See Appendix A).
- ^d Based on equation: 10 S + 3, where S =sulfur content. PM10 is 71% of PM emissions.
- ^c Based on equation: 157 S, where S = sulfur content.
- Nitrogen oxides emissions based on ratio of residual and distillate oil emission factors [67 lb/10³ gallons x 20 lb/10³ gallons (for distillate) ÷ 55 lb/10³ gallons (for residual)].

Table 2-6. Net Emission Reductions From Boilers 1 Through 5 at UF Central Heating Plant

		Emission Reduction (TPY)
Dallutant	Boilers ^a	Boilers ^b	Total
Pollutant	1, 2 and 3	4 and 5	1 Otai
Particulate Matter	-1.00	-3.13	-4.13
Particulate Matter (PM10)	-0.96	-2.42	-3.38
Sulfur Dioxide	-1.99	-34.08	-36.07
Nitrogen Oxides	-72.18	-62.69	-134.87
Carbon Monoxide	-11.04	-9.38	-20.41
Volatile Organic			
Compounds (methane)	-0.37	-0.31	-0.67
Volatile Organic			
Compounds (nonmethane)	-0.55	-0.49	-1.05
Lead	-0.0000	-0.0004	-0.0004
Fluorides	-0.0003	-0.0051	-0.0054
Mercury	-0.00000	-0.00	-0.00
Beryllium	-0.00000	-0.00006	-0.00006
Arsenic	-0.0000	-0.0003	-0.0003
Sulfuric Acid Mist	-0.0411	-0.7366	-0.7777

Note: TPY = tons per year.

^aBased on emissions in Table 2-3. ^bBased on subtracting emissions in Table 2-4 from emissions in Table 2-5.

3.4.2 PSD REVIEW

3.4.2.1 Pollutant Applicability

The proposed project is considered to be a modification to a major facility because the facility is listed as one of the "List of 28" and potential emissions of any regulated pollutant exceed 100 TPY; therefore, PSD review is required for any pollutant for which the net increase in emissions exceeds the PSD significant emission rates presented in Table 3-2 (i.e., major modification). As shown, potential emissions from the proposed project will exceed the PSD significant emission rate for CO. Therefore, the project is subject to PSD review for this pollutant.

Table 3-3. Net Increase in Emissions Due To the UF Cogeneration Facility Compared to the PSD Significant Emission Rates

		<u>Emi</u>	ssions (TPY)		
En	Potential nissions From Proposed Project	Net Emission Reduction From Boilers 1-5	Net Emissions Increase	Significant Emission Rate	PSD Review
Sulfur Dioxide	26.6	36.1	-9.5	40	No
Particulate Matter (TSP)	13.8	4.1	9.7	25	No
articulate Matter (PM10)	13.8	3.4	10.4	15	No
litrogen Dioxide	174.6	134.9	39.7	40	No
Carbon Monoxide	326.7	20.4	306.3	100	Yes
olatile Organic Compoun	ds 17.5	1.05	16.5	40	No
ead	0.00034	0.0004	0.0002	0.6	No
ulfuric Acid Mist	2.4	0.78	1.6	7	No
otal Fluorides	0.0014	0.0054	-0.004	3	No
Cotal Reduced Sulfur	Neg	Neg	Neg	10	No
Reduced Sulfur Compound	ls* Neg	Neg	Neg	10	No
Hydrogen Sulfide	Neg	Neg	Neg	10	No
Asbestos*	Neg	Neg	Neg	0.007	No
Beryllium	0.00011	0.00006	0.00004	0.0004	No
Mercury	0.00013	Neg	0.00013	0.1	No
/inyl Chloride*	Neg	Neg	Neg	1	No
Benzene ^a	Neg	Neg	Neg	_ • 0	No
Radionuclides*	Neg	Neg	Neg	0	No
norganic Arsenic	0.00018	0.0003	-0.00012	0	No

Note: Neg = Negligible.

TPY = tons per year.

All calculations based on 59°F peak load condition.

^{*}Emissions of these pollutants considered not to have any emission rate increase.

APPENDIX A

Table A-1. Design Information and Stack Parameters for University of Florida Cogeneration Project

Data	Gas Turbine Natural Gas	Duct Burner Natural Gas	Gas Turbine Fuel Oil
A	В	C	D
General:			
Power (kW)	43,262.0	NA	43,098.0
Heat Rate (Btu/kwh)	8,043.0	NA	8,877.0
leat Input (mmBtu/hr)	348.0	187.0	382.6
Fuel Oil (lb/hr)	18,313.5	9,842.1	20,792.4
(cf/hr)	367,818.5	197,674.4	
Fuel:			
Heat Content - (LHV)	19,000 Btu/lb	19,000 Btu/lb	18,400 Btu/lb
Sulfur	1 gr/100cf	1 gr/100cf	0.5
CT Exhaust:			
Volume Flow (acfm)	564,678		569,684
Volume Flow (scfm)	239,478		235,916
Mass Flow (lb/hr)	1,036,522		1,030,290
Temperature (oF)	785		815
Moisture (% Vol.)	. 11.25		8.54
Oxygen (% Vol.)	13.73		13.60
Molecular Weight	27.80		28.05
Steam Injected (lb/hr)	31,402		22,504
HRSG Stack:			
Volume Flow (acfm)	325,200		320,364
Temperature (oF)	257		257
Diameter (ft)	10		9.8
Velocity (ft/sec)	72.59		71.5

Source: General Electric and Stewart and Stevenson, 1991.

Note: All data shown on this table and subsequent tables are for the combustion turbine and duct burner.

>."

Pollutant	Gas Turbine	Duct Burner	Gas Turbine
A	Natural Gas B	Natural Gas C	Fuel Oil D
Particulate:			
Basis	Manufacturer	0.01 lb/mmBtu	Manufacturer
lb/hr	2.50	1.87	10.0
TPY	10.95	2.46	1.1
Sulfur Dioxide:			
Basis	1 gr/100 cf	1 gr/100 cf	0.5 % Sulfur
lb/hr	1.05	0.56	197.53
TPY	4.60	0.74	21.6
Nitrogen Oxides:			
Basis	25 ppm*	0.1 lb/mmBtu	42 ppm*
lb/hr	35.0	18.7	66.3
TPY	153.4	24.57	7.3
ppm	25.0	NA	42.0
Carbon Monoxide:			
Basis	75 ppm+	0.15 lb/mmBtu	75 ppm+
lb/hr	69.5	28.1	70.5
TPY	304.37	36.86	7.7
ppm	75.0	NA	75.0
VOC's:			
Basis	4 ppm+	0.043 lb/mmBtu	10 ppm+
lb/hr	1.59	8.04	4.03
TPY	7.0	10.57	0.4
ppm	4.0	NA	10.0
Lead:			
Basis			EPA(1988)
lb/hr	NA	- NA	3.40E-03
TPY	NA	NA	3.73E-04

^{*} corrected to 15% 02 dry conditions

Note: Annual emission for CT when firning natural gas based on 8,760 hrs/yr and 219 hrs/yr for fuel oil firing. Annual emissions for duct burners on 2,628 hrs/yr (30% capacity factor).

⁺ corrected to dry conditions

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Table A-3. Maximum Other Regulated Pollutant Emissions for UF Cogeneration Project

Pollutant	Gas Turbine Natural Gas B	Duct Burner Natural Gas C	Gas Turbine No.2 Oil
A	D		D
As (lb/hr)	NEG.	NEG.	0.0016068399732
(TPY)	NEG.	NEG.	1.76E-04
Be (lb/hr)	NEG.	NEG.	0.000956452365
(TPY)	NEG.	NEG.	1.05E-04
Hg (lb/hr)	NEG.	NEG.	1.15E-03
(TPY)	NEG.	NEG.	1.26E-04
F (lb/hr)	NEG.	NEG.	0.012433880745
(TPY)	NEG.	NEG.	1.36E-03
H2SO4 (1b/hr)	8.04E-02	4.32E-02	1.51E+01
(TPY)	3.52E-01	0.06	1.65E+00

Sources: EPA, 1988; EPA, 1980

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Table A-4. Maximum Non-Regulated Pollutant Emissions for UF Cogeneration Project

Pollutant	Gas Turbine Natural Gas	Duct Burner Natural Gas	Gas Turbine No.2 Oil
Α	В	С	D
Manganese (lb/hr)	NEG.	NEG.	2.46E-03
(TPY)	NEG.	NEG.	2.70E-04
Nickel (lb/hr)	NEG.	NEG.	6.50E-02
(TPY)	NEG.	NEG.	7.12E-03
Cadmium (lb/hr)	NEG.	NEG.	4.02E-03
(TPY)	NEG.	NEG.	4.40E-04
Chromium (lb/hr)	NEG.	NEG.	1.82E-02
(TPY)	NEG.	NEG.	1.99E-03
Copper (lb/hr)	NEG.	NEG.	1.07E-01
(TPY)	NEG.	NEG.	1.17E-02
Vanadium (lb/hr)	NEG.	NEG.	2.67E-02
(TPY)	NEG.	NEG.	2.92E-03
Selenium (lb/hr)	NEG.	NEG.	8.98E-03
(TPY)	NEG.	NEG.	9.83E-04
POM (lb/hr)	3.88E-04	2.09E-04	1.07E-04
(TPY)	1.70E-03	2.74E-04	1.17E-05
Formaldehyde (lb/hr)	3.07E-02	7.57E-02	1.55E-01
(TPY)	1.35E-01	9.95E-02	1.70E-02

Source: EPA, 1988.

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Table A-5. Maximum Emissions for Additional Non-Regulated Pollutant for UF Cogeneration Project

Pollutant	Gas Turbine Natural Gas	Duct Burner Natural Gas	Gas Turbine No.2 Oil
A	В	С	D
Antimony (lb/hr)	NEG.	NEG.	8.36E-03
(TPY)	NEG.	NEG.	9.15E-04
Barium (lb/hr)	NEG.	NEG.	7.47E-03
(TPY)	NEG.	NEG.	8.18E-04
Colbalt (lb/hr)	NEG.	NEG.	3.47E-03
(TPY)	NEG.	NEG.	3.80E-04
Zinc (lb/hr)	NEG.	NEG.	2.61E-01
(TPY)	NEG.	NEG.	2.86E-02
Chlorine^a (lb/hr)	NEG.	NEG.	1.04E-02
(TPY)	NEG.	NEG.	1.14E-03

Source: EPA, 1979

[^]a Assumes 0.5 ppm in fuel oil.

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A:A1: [W24] 'Table A-1. Design Information and Stack Parameters for University of Florida (UF)
A:E1: [W6] 1
             Cogeneration Project
A:A2: [W24] '
A:E2: [W6] (E1+1)
A:A3: [W24] \_
A:B3: {W18} \_
A:C3: [W18] \_
A:03: [W18] \_
A:E3: [W6] (E2+1)
A:E4: [W6] (E3+1)
A:A5: [W24] ^Data
A:B5: [W18] "Gas Turbine
A:C5: [W18] "Duct Burner
A:D5: [W18] "Gas Turbine
A:E5: [W6] (E4+1)
A:B6: [W18] "Natural Gas
A:C6: [W18] "Natural Gas
A:D6: [W18] "Fuel Oil
A:E6: [W6] (E5+1)
A:A7: [W24] ^A
A:B7: [W18] "B
A:C7: [W18] "C
A:D7: [W18] "D
A:E7: [W6] (E6+1)
A:A8: [W24] \_
A:B8: [W18] \_
A:C8: [W18] \_
A:D8: [W18] \_
A:E8: [W6] (E7+1)
A:E9: [W6] (E8+1)
A:A10: [W24] ^General:
A:E10: [W6] (E9+1)
A:A11: [W24] 'Power (kW)
A:C11: (,1) [W18] "NA
A:E11: [W6] (E10+1)
A:A12: [W24] 'Heat Rate (Btu/kwh)
A:B12: (,1) [W18] 8043 ..... From GE
A:C12: (,1) [W18] "NA
A:D12: (,1) [W18] 8877
             A:E12: [W6] (E11+1)
A:A13: [W24] 'Reat Input (mmBtu/hr)
A:E13: [W6] (E12+1)
A:A14: [W24] 'Fuel Oil (lb/hr)
A:C14: (,1) [W18] (C13/0.019)
A:D14: (,1) [W18] (D13/0.0184)
A:E14: [W6] (E13+1)
A:A15: [W24] '
             (cf/hr)
A:B15: (,1) [W18] (B13/946*10^6) ...... Heat Input + Heat Content
A:C15: (,1) [W18] (C13/946*10^6)
A:E15: [W6] (E14+1)
A:E16: [W6] (E15+1)
A:A17: [W24] ^Fuel:
A:E17: [W6] (E16+1)
A:A18: [W24] 'Heat Content - (LHV)
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A:C18: (,1) [W18] "19,000 Btu/lb
A:D18: (,1) [W18] "18,400 Btu/lb
A:E18: [W6] (E17+1)
A:A19: [W24] 'Sulfur
A:C19: (.1) [W18] #1 gr/100cf
A:E19: [W6] (E18+1)
A:E20: [W6] (E19+1)
A:A21: [W24] ^CT Exhaust:
A:E21: [W6] (E20+1)
A:A22: [W24] 'Volume Flow (acfm)
A:D22: (,0) [W18] (D24*1545*(460+D25)/(D28*2116.8*60))
A:E22: [W6] (E21+1)
A:A23: [W24] 'Volume Flow (scfm)
A:D23: (.0) [W18] (D24*1545*(460+68)/(D28*2116.8*60))
A:E23: [W6] (E22+1)
A:A24: [W24] 'Mass Flow (lb/hr)
A:D24: (,0) [W18] 1030290
A:E24: [W6] (E23+1)
A:A25: [W24] 'Temperature (oF)
A:D25: (,0) [W18] 815
A:E25: [W6] (E24+1)
                 . . .
A:A26: [W24] 'Moisture (% Vol.)
A:D26: (F2) [W18] 8.54
A:E26: [W6] (E25+1)
A:A27: [W24] 'Oxygen (% Vol.)
A:D27: (F2) [W18] 13.6
A:E27: [W6] (E26+1)
A:A28: [W24] 'Molecular Weight
A:B28: (F2) [W18] 27.8 . . . . .
                 ....... Calculated from GE
A:D28: (F2) [W18] 28.05
A:E28: [W6] (E27+1)
A:A29: [W24] 'Steam Injected (lb/hr)
A:D29: (,0) [W18] 22504
A:E29: [W6] (E28+1)
A:E30: [W6] (E29+1)
A:A31: [W24] ^HRSG Stack:
A:E31: [W6] (E30+1)
A:A32: [W24] 'Volume Flow (acfm)
A:D32: (,0) [W18] (D22*(D33+460)/(D25+460))
A:E32: [W6] (E31+1)
A:A33: [W24] 'Temperature (of)
A:D33: (,0) [W18] 257
A:E33: [W6] (E32+1)
A:A34: [W24] 'Diameter (ft)
A:B34: (F0) [W18] 9.75
A:034: (,1) [W18] 9.75
A:E34: [W6] (E33+1)
A:A35: [W24] 'Velocity (ft/sec)
A:D35: (F2) [W18] (D32/60/(D34^2*3.14159/4))
A:E35; [W6] (E34+1)
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A:E36: [W6] (E35+1)

A:A37: [W24] \_
A:B37: [W18] \_
A:C37: [W18] \_
A:D37: [W18] \_
A:E37: [W6] (E36+1)

A:E38: [W6] (E37+1)

A:A39: [W24] 'Source: General Electric and Stewart and Stevenson, 1991.

A:E39: [W6] (E38+1)

A:A40: [W24] 'Note: All data shown on this table and subsequent tables are for each A:E40: [W6] (E39+1)

A:A41: [W24] ' combustion turbine and duct burner.

A:E41: [W6] (E40+1)
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A:A47: [W24] 'Table A-2. Maximum Criteria Pollutant Emissions for
A:E47: [W6] 47
A:A48: [W24] '
                     Cogeneration Project
A:E48: [W6] (E47+1)
A:A49: [W24] \_
A:B49: [W18] \_
A:C49: [W18] \_
A:D49: [W18] \_
A:E49: [W6] (E48+1)
A:E50: [W6] (E49+1)
A:A51: [W24] ^Pollutant
A:B51: [W18] "Gas Turbine
A:C51: [W18] "Duct Burner
A:051: [W18] "Gas Turbine
A:E51: [W6] (E50+1)
A:B52: [W18] "Natural Gas
A:C52: [W18] "Natural Gas
A:D52: [W18] "Fuel Oil
A:E52: [W6] (E51+1)
A:A53: [W24] ^A
A:B53: [W18] "B
A:C53: [W18] "C
A:D53: [W18] "D
A:E53: [W6] (E52+1)
A:A54: [W24] \_
A:B54: [W18] \_
A:C54: [W18] \_
A:D54: [W18] \
A:E54: [W6] (E53+1)
A:E55: [W6] (E54+1)
A:A56: [W24] 'Particulate:
A:E56: [W6] (E55+1)
A:A57: [W24] ' Basis
A:B57: (,1) [W18] "Manufacturer
A:C57: (,1) [W18] "0.01 lb/mm8tu
A:D57: (,1) [W18] "Manufacturer
A:E57: [W6] (E56+1)
A:A58: [W24] ' lb/hr
A:E58: [W6] (E57+1)
A:A59: [W24] ' TPY
A:B59: (F2) [W18] (B58*8760/2000) . . . . . . . . . . . . . Emissions * 8,760 hours/year ÷ 2,000 lb/ton
A:C59: (F2) [W18] (C58*4.38*0.3) . . . . . . . . . . . . . Emissions-* 4.38 TPY/lb/hr ÷ 0.3 Capacity Factor
A:D59: (,1) [W18] (D58*219/2000) . . . . . . . . . . . . . . Emissions * 219 hours/year ÷ 2,000 lb/ton
A:E59: [W6] (E58+1)
A:E60: [W6] (E59+1)
A:A61: [W24] 'Sulfur Dioxide:
A:E61: [W6] (E60+1)
A:A62: [W24] ' Basis
A:B62: (,1) [W18] "1 gr/100 cf
A:C62: (,1) [W18] "1 gr/100 cf
A:D62: (,1) [W18] "0.5 % Sulfur
A:E62: [W6] (E61+1)
A:A63: [W24] ' lb/hr
A:863: (F2) [W18] (B15*1/7000*2/100)
                               . . . . . . . . Fuel Used (CF/HR) * Sulfur Content * 2 lb SO,/lb S * 1/100 CF
A:C63: (F2) [W18] (C15*1/7000*2/100)
A:D63: (F2) [W18] (D14*0.005*2*0.95) ..... Fuel Used (lb/hr) * Sulfur Content * 2 lb S0;/lb S * 95% Emitted
A:E63: [W6] (E62+1)
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A:A64: [W24] ' TPY

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A:B64: (F2) [W18] (B63*8760/2000)
A:C64: (F2) [W18] (C63*4.38*0.3)
A:D64: (,1) [W18] (D63*219/2000)
A:E64: [W6] (E63+1)
A:E65: [W6] (E64+1)
A:A66: [W24] 'Nitrogen Oxides:
A:E66: [W6] (E65+1)
A:A67: [W24] ' Basis
A:B67: (,1) [W18] "25 ppm*
A:C67: (,1) [W18] "0.1 lb/mm8tu
A:D67: (,1) [W18] "42 ppm*
A:E67: [W6] (E66+1)
A:A68: [WZ4] ' lb/hr
A:B68: (,1) [W18] (B70/5.9*(20.9*(1-B26/100)-B27)*B22*2116.8*46*60/(1545*(460+B25)*1000000)) . . . . . . . See Note B
A:D68: (,1) [W18] (D70/5.9*(20.9*(1-D26/100)-D27)*D22*2116.8*46*60/(1545*(460+D25)*1000000)) ..... See Note B
A:E68: [W6] (E67+1)
A:A69: [W24] ' TPY
A:B69: (F1) [W18] (B68*8760/2000)
A:C69: (F2) [W18] (C68*4.38*0.3)
A:D69: (,1) [W18] (D68*219/2000)
A:E69: [W6] (E68+1)
A:A70: [W24] ' ppm
A:C70: (,1) [W18] "NA
A:D70: (,1) [W18] 42 ..... From GE
A:E70: [W6] (E69+1)
A:E71: [W6] (E70+1)
A:A72: [W24] 'Carbon Monoxide:
A:E72: [W6] (E71+1)
A:A73: [W24] ' Basis
A:B73: (,1) [W18] "75 ppm+ . . . . . . . . . . . From GE
A:E73: [W6] (E72+1)
A:A74: [W24] / lb/hr
A:D74: (,1) [W18] (D76*(1-D26/100)*D22*2116.8*28*60/(1545*(460+D25)*1000000)) . . . . . . . . . . . . . See Note C
A:E74: [W6] (E73+1)
A:A75: [W24] ' TPY
A:B75: (FZ) [W18] (B74*8760/2000)
A:C75: (F2) [W18] (C74*4.38*0.3)
A:D75: (,1) [W18] (D74*219/2000)
A:E75: [W6] (E74+1)
A:A76: [W24] ' ppm
A:B76: (,1) [W18] 75
A:C76: (,1) [W18] "NA
A:D76: (,1) [W18] 75
A:E76: [W6] (E75+1)
A:E77: [W6] (E76+1)
A:A78: [W24] 'VOC's:
A:E78: [W6] (E77+1)
A:A79: [W24] ' Basis
A:879: (,1) [W18] "4 ppm+
A:C79: (,1) [W18] "0.043 lb/mmBtu
A:D79: (,1) [W18] "10 ppm+
A:E79: [W6] (E78+1)
A:A80: [W24] ' lb/hr
A:C80: (F2) [W18] (C13*0.043)
A:D80: (F2) [W18] (D82*(1-D26/100)*D22*2116.8*12*60/(1545*(460+D25)*1000000)) . . . . . . . . . . . . . . See Note C
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A:E80: [W6] (E79+1)
 A:A81: [W24] ' TPY
A:B81: (,1) [W18] (B80*8760/2000)
A:C81: (F2) [W18] (C80*4.38*0.3)
A:D81: (,1) [W18] (D80*219/2000)
A:E81: [W6] (E80+1)
A:A82: [W24] / ppm
A:B82: (,1) [W18] 4
A:C82: (,1) [W18] "NA
A:D82: (,1) [W18] 10
A:E82: [W6] (E81+1)
A:E83: [W6] (E82+1)
A:A84: [W24] 'Lead:
A:E84: [W6] (E83+1)
A:A85: [W24] ' Basis
A:D85: [W18] "EPA(1988)
A:E85: [W6] (E84+1)
A:A86: [W24] / lb/hr
A:B86: (S2) [W18] "NA
A:C86: (S2) [W18] "NA
A:D86: (S2) [W18] (D13*8.9/1000000) . . . . . . . . . . . From EPA 1988; Page 4-156; Heat Input * Emission Factor
A:E86: [W6] (E85+1)
A:A87: [W24] ' TPY
A:887: (S2) [W18] "NA
A:C87: (S2) [W18] "NA
A:D87: (S2) [W18] (D86*219/2000)
A:E87: [W6] (E86+1)
A:A88: [W24] \_
A:B88: [W18] \_
A:C88: [W18] \_
A:D88: [W18] \_
A:E88: [W6] (E87+1)
A:E89: [W6] (E88+1)
A:A90: [W24] /* corrected to 15% 02 dry conditions
A:E90: [W6] (E89+1)
A:A91: [W24] '+ corrected to dry conditions
A:E91: [W6] (E90+1)
A:A92: [W24] 'Note: Annual emission for CT when firning natural gas based on 8,760 hrs/yr
A:E92: [W6] (E91+1)
A:A93: [W24] /
                 and 219 hrs/yr for fuel oil firing. Annual emissions for duct burners
A:E93: [W6] (E92+1)
A:A94: [W24] ' on 2,628 hrs/yr (30% capacity factor).
A:E94: [W6] (E93+1)
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A:A96: [W24] 'Table A-3. Maximum Other Regulated Pollutant Emissions for UF
A:E96: [W6] 96
A:A97: [W24] '
                    Cogeneration Project
A:E97: [W6] (E96+1)
A:A98: [W24] \_
A:898: [W18] \_
A:C98: [W18] \_
A:D98: [W18] \_
A:E98: [W6] (E97+1)
A:E99: [W6] (E98+1)
A:A100: [W24] ^Pollutant
A:B100: [W18] "Gas Turbine
A:C100: [W18] "Duct Burner
A:D100: [W18] "Gas Turbine
A:E100: [W6] (E99+1)
A:B101: [W18] "Natural Gas
A:C101: [W18] "Natural Gas
A:D101: [W18] "No.2 Oil
A:E101: [W6] (E100+1)
A:A102: [W24] ^A
A:B102: [W18] "B
A:C102: [W18] "C
A:D102: [W18] "D
A:E102: [W6] (E101+1)
A:A103: [W24] \_
A:B103: [W18] \_
A:C103: [W18] \_
A:D103: [W18] \
A:E103: [W6] (E102+1)
A:E104: [W6] (E103+1)
A:A105: [W24] ' As (lb/hr)
A:B105: [W18] "NEG.
A:C105: [W18] "NEG.
A:E105: [W6] (E104+1)
A:A106: [W24] ' (TPY)
A:B106: [W18] "NEG.
A:C106: [W18] "NEG.
A:D106: (S2) [W18] (D105*219/2000)
A:E106: [W6] (E105+1)
A:E107: [W6] (E106+1)
A:A108: [W24] ' Be (lb/hr)
A:B108: [W18] "NEG.
A:C108: [W18] "NEG.
A:E108: [W6] (E107+1)
A:A109: [W24] /
             (TPY)
A:B109: [W18] "NEG.
A:C109: [W18] "NEG.
A:D109: (S2) [W18] (D108*219/2000)
A:E109: [W6] (E108+1)
A:E110: [W6] (E109+1)
A:A111: [W24] ' Hg (lb/hr)
A:B111: [W18] "NEG.
A:C111: [W18] "NEG.
A:E111: [W6] (E110+1)
A:A112: [W24] /
                (TPY)
A:B112: [W18] "NEG.
A:C112: [W18] "NEG.
A:D112: (S2) [W18] (D111*219/2000)
A:E112: [W6] (E111+1)
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A:E113: [W6] (E112+1)
A:A114: [W24] ' F (lb/hr)
A:8114: [W18] "NEG.
A:C114: [W18] "NEG.
A:D114: [W18] (D13*32.5/1000000) . . . . . . . . From EPA 1981; Table 6-1, 2.324 pq/J * 14 pq/J = 32.5 lb/10 BTU
A:E114: [W6] (E113+1)
A:A115: [W24] ' (TPY)
A:B115: [W18] "NEG.
A:C115: [W18] "NEG.
A:D115: (S2) [W18] (D114*219/2000)
A:E115: [W6] (E114+1)
A:E116: [W6] (E115+1)
A:A117: [W24] ' H2S04 (lb/hr)
A:C117: (S2) [W18] (C63*0.05*3.06/2) . . . S0, emissions * %H<sub>2</sub>SO, formed (5%) * MW<sub>rasos</sub>/MW<sub>sox</sub> * correction to total S0,
A:D117: (S2) [W18] (D63*0.05*3.06/2)
A:E117: [W6] (E116+1)
A:A118: [W24] ' (TPY)
A:B118: (S2) [W18] (8117*8760/2000)
A:C118: (F2) [W18] (C117*4.38*0.3)
A:D118: (S2) [W18] (D117*219/2000)
A:E118: [W6] (E117+1)
A:E119: [W6] (E118+1)
A:A120: [W24] \_
A:B120: [W18] \_
A:C120: [W18] \_
A:D120: [W18] \_
A:E120: [W6] (E119+1)
A:E121: [W6] (E120+1)
A:A122: [W24] 'Sources: EPA, 1988; EPA, 1980
A:E122: [W6] (E121+1)
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A:A125: [W24] 'Table A-4. Maximum Non-Regulated Pollutant Emissions for UF
A:E125: [W6] 125
A:A126: [W24] '
                     Cogeneration Project
A:E126: [W6] (E125+1)
A:A127: [W24] \_
A:B127: [W18] \_
A:C127: [W18] \_
A:D127: [W18] \_
A:E127: [W6] (E126+1)
A:E128: [W6] (E127+1)
A:A129: [W24] ^Pollutant
A:B129: [W18] "Gas Turbine
A:C129: [W18] "Duct Burner
A:D129: [W18] "Gas Turbine
A:E129: [W6] (E128+1)
A:B130: [W18] "Natural Gas
A:C130: [W18] "Natural Gas
A:D130: [W18] "No.2 Oil
A:E130: [W6] (E129+1)
A:A131: [W24] ^A
A:B131: [W18] "B
A:C131: [W18] "C
A:D131: [W18] "D
A:E131: [W6] (E130+1)
A:A132: [W24] \_
A:B132: [W18] \_
A:C132: [W18] \_
A:D132: [W18] \_
A:E132: [W6] (E131+1)
A:E133: [W6] (E132+1)
A:A134: [W24] / Manganese (lb/hr)
A:B134: [W18] "NEG.
A:C134: [W18] "NEG.
A:E134: [W6] (E133+1)
A:A135: [W24] '
               (TPY)
A:B135: [W18] "NEG.
A:C135: [W18] "NEG.
A:D135: (S2) [W18] (D134*219/2000)
A:E135: [W6] (E134+1)
A:E136: [W6] (E135+1)
A:A137: [W24] ' Nickel (lb/hr)
A:B137: [W18] "NEG.
A:C137: [W18] "NEG.
A:E137: [W6] (E136+1)
A:A138: [W24] /
               (TPY)
A:B138: [W18] "NEG.
A:C138: [W18] "NEG.
A:D138: (S2) [W18] (D137*219/2000)
A:E138: [W6] (E137+1)
A:E139: [W6] (E138+1)
A:A140: [W24] ' Cadmium (lb/hr)
A:B140: [W18] "NEG.
A:C140: [W18] "NEG.
A:E140: [W6] (E139+1)
A:A141: [W24] '
A:B141: [W18] "NEG.
A:C141: [W18] "NEG.
A:D141: (S2) [W18] (D140*219/2000)
A:E141: [W6] (E140+1)
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A:E142: [W6] (E141+1)
A:A143: [W24] ' Chromium (lb/hr)
A:B143: [W18] "NEG.
A:C143: [W18] "NEG.
A:E143: [W6] (E142+1)
A:A144: [W24] ' (TPY)
A:B144: [W18] "NEG.
A:C144: [W18] "NEG.
A:D144: (S2) [W18] (D143*219/2000)
A:E144: [W6] (E143+1)
A:E145: [W6] (E144+1)
A:A146: [W24] ' Copper (lb/hr)
A:B146: [W18] "NEG.
A:C146: [W18] "NEG.
A:E146: [W6] (E145+1)
A:A147: [W24] ' (TPY)
A:B147: [W18] "NEG.
A:C147: [W18] "NEG.
A:D147: (S2) [W18] (D146*219/2000)
A:E147: [W6] (E146+1)
A:E148: [W6] (E147+1)
A:A149: [W24] ' Vanadium (lb/hr)
A:B149: [W18] "NEG.
A:C149: [W18] "NEG.
A:D149: (S2) [W18] (D13*30*2.324/1000000) . . . . . . . . From EPA 1988, See Page 4-162; 2.324 pq/J = 1 lb/10* BTU
A:E149: [W6] (E148+1)
A:A150: [W24] '
               (TPY)
A:B150: [W18] "NEG.
A:C150: [W18] "NEG.
A:D150: (S2) [W18] (D149*219/2000)
A:E150: [W6] (E149+1)
A:E151: [W6] (E150+1)
A:A152: [W24] ' Selenium (lb/hr)
A:B152: [W18] "NEG.
A:C152: [W18] "NEG.
A:E152: [W6] (E151+1)
A:A153: [W24] ' (TPY)
A:B153: [W18] "NEG.
A:C153: [W18] "NEG.
A:D153: (S2) [W18] (D152*219/2000)
A:E153: [W6] (E152+1)
A:E154: [W6] (E153+1)
A:A155: [W24] ' POM (lb/hr)
A:B155: (S2) [W18] ($B$13*0.48*2.324/1000000) . . . . . . . . . . . . . . . From EPA 1988, See Page 4-161
A:C155: (S2) [W18] ($C$13*0.48*2.324/1000000)
A:D155: (S2) [W18] ($D$13*0.12*2.324/1000000)
A:E155: [W6] (E154+1)
A:A156: [W24] '
             (TPY)
A:B156: (S2) [W18] (B155*8760/2000)
A:C156: (S2) [W18] (C155*4.38*0.3)
A:D156: (S2) [W18] (D155*219/2000)
A:E156: [W6] (E155+1)
A:E157: [W6] (E156+1)
A:A158: [W24] ' Formaldehyde (lb/hr)
A:C158: (S2) [W18] ($C$13*405/1000000)
A:D158: ($2) [W18] ($D$13*405/1000000)
A:E158: [W6] (E157+1)
A:A159: [W24] ' (TPY)
```

```
A:B159: (S2) [W18] (B158*8760/2000)
A:C159: (S2) [W18] (C158*4.38*0.3)
A:D159: (S2) [W18] (D158*219/2000)
A:E159: [W6] (E158+1)
A:A160: [W24] \_
A:B160: [W18] \_
A:C160: [W18] \_
A:D160: [W18] \_
A:E160: [W6] (E159+1)
A:E161: [W6] (E160+1)
A:E162: [W6] (E161+1)
```

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A:A165: [W24] 'Table A-5. Maximum Emissions for Additional Non-Regulated Pollutant
A:E165: [W6] 165
A:A166: [W24] '
                     for UF Cogeneration Project
A:E166: [W6] (E165+1)
A:A167: [W24] \_
A:B167: [W18] \_
A:C167: [W18] \_
A:D167: [W18] \
A:E167: [W6] (E166+1)
A:E168: [W6] (E167+1)
A:A169: [W24] ^Pollutant
A:B169: [W18] "Gas Turbine
A:C169: [W18] "Duct Burner
A:D169: [W18] "Gas Turbine
A:E169: [W6] (E168+1)
A:8170: [W18] "Natural Gas
A:C170: [W18] "Natural Gas
A:D170: [W18] "No.2 Oil
A:E170: [W6] (E169+1)
A:A171: [W24] ^A
A:B171: [W18] "B
A:C171: [W18] "C
A:D171: [W18] "D
A:E171: [W6] (E170+1)
A:A172: [W24] \_
A:B172: [W18] \_
A:C172: [W18] \_
A:D172: [W18] \_
A:E172: [W6] (E171+1)
A:E173: [W6] (E172+1)
A:A174: [W24] ' Antimony (lb/hr)
A:B174: [W18] "NEG.
A:C174: [W18] "NEG.
A:E174: [W6] (E173+1)
A:A175: [W24] ' (TPY)
A:B175: [W18] "NEG.
A:C175: [W18] "NEG.
A:D175: ($2) [W18] (D174*219/2000)
A:E175: [W6] (E174+1)
A:E176: [W6] (E175+1)
A:A177: [W24] ' Barium (lb/hr)
A:B177: [W18] "NEG.
A:C177: [W18] "NEG.
A:E177: [W6] (E176+1)
A:A178: [W24] ' (TPY)
A:B178: [W18] "NEG.
A:C178: [W18] "NEG.
A:D178: (S2) [W18] (D177*219/2000)
A:E178: [W6] (E177+1)
A:E179: [W6] (E178+1)
A:A180: [W24] ' Colbalt (lb/hr)
A:8180: [W18] "NEG.
A:C180: [W18] "NEG.
A:E180: [W6] (E179+1)
A:A181: [W24] '
               (TPY)
A:B181: [W18] "NEG.
A:C181: [W18] "NEG.
A:D181: (S2) [W18] (D180*219/2000)
A:E181: [W6] (E180+1)
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A:E182: [W6] (E181+1)
A:A183: [W24] ' Zinc (lb/hr)
A:B183: [W18] "NEG.
A:C183: [W18] "NEG.
A:D183: (S2) [W18] ($D$13*294*2.324/1000000) ................ From EPA 1979, See Page 137
A:E183: [W6] (E182+1)
A:A184: [W24] ' (TPY)
A:B184: [W18] "NEG.
A:C184: [W18] "NEG.
A:D184: (S2) [W18] (D183*219/2000)
A:E184: [W6] (E183+1)
A:E185: [W6] (E184+1)
A:A186: [W24] ' Chlorine^a (lb/hr)
A:B186: [W18] "NEG.
A:C186: [W18] "NEG.
A:E186: [W6] (E185+1)
A:A187: [W24] ' (TPY)
A:B187: [W18] "NEG.
A:C187: [W18] "NEG.
A:D187: (S2) [W18] (D186*219/2000)
A:E187: [W6] (E186+1)
A:A188: [W24] \_
A:8188: [W18] \_
A:C188: [W18] \_
A:D188: [W18] \_
A:E188: [W6] (E187+1)
A:E189: [W6] (E188+1)
A:A190: [W24] 'Source: EPA, 1979
A:E190: [W6] (E189+1)
A:A191: [W24] ' ^a Assumes 0.5 ppm in fuel oil.
A:E191: [W6] (E190+1)
```

EMISSION FACTORS AND CALCULATIONS

Emission factors used in the calculations were obtained from the following sources (references attached):

- 1. Compilation of air pollutant emission factors (AP-42) for PM, SO_2 , NO_x , CO, and VOC.
- 2. Estimating air toxics from coal and oil combustion sources (EPA, 1989) for As, Be, Pb, and Hg.
- 3. Emissions Assessment of Conventional Stationary Combustion Systems: Volume V: Industrial Combustion Sources (EPA, 1981) for F.

The conversions from $1b/10^{-12}$ Btu to $1b/10^3$ gal were calculated as follows:

Residual Oil = EF $1b/10^{12}$ Btu * 18,300 Btu/lb oil * 8.2 lb oil/gal

$$*1,000/10^3 = 1.5 \times 10^{-4} * EF lb/10^3 gal$$

where: EF - emission factor

Distillate Oil = EF $1b/10^{12}$ Btu * 20,996/1b oil * 7.2 1b/gal

*
$$1,000/10^3 - 1.512 \times 10^{-4} \times EF lb/10^3 gal$$

The conversion from pg/J to $1b/10^{12}$ Btu is as follows:

 $pg/J * 10^{-12} g/pg * lb/454 grams * 1,055 J/Btu = 2.324 lb/10^{12} Btu$

Α

Volume is calculated based on ideal gas law:

PV - mRT/M

V = mRT/(MP) for natural gas

where: P = pres

 $P = pressure = 2116.8 lb/ft^2$

m = mass flow of gas (lb/hr)

R - universal gas constant - 1545 ft-lb/lb-mole °R

M - molecular weight of gas

T - temperature (K)

В

 ${\rm NO_x}$ is calculated by correcting to 15% ${\rm O_2}$ dry conditions using ideal gas law and moisture and ${\rm O_2}$ conditions.

Oxygen correction:

$$V_{NOx (15X)} - V_{NOx Dry} * 5.9$$

$$\frac{1}{20.9 - \chi_{O_{2 Dry}}}$$

$$V_{NOx Dry} - V_{NOx (15X)} (20.9 - \chi_{O_{2 Dry}}) / 5.9$$

$$\chi_{O_{2 Dry}} - \chi_{O_{2 Act}} / (1 - \chi_{H_{2}O}) ; \chi_{O_{2 Act}} - \chi_{O_{2 Dry}} (1 - \chi_{H_{2}O})$$

$$V_{NOx Act} - V_{NOx Dry} (1 - \chi_{H_{2}O})$$

Substituting:

$$V_{NOx Act} = V_{NOx 15x} (20.9 - xO_{2 Dry}) (1 - xH_{2}O) / 5.9$$

$$= V_{NOx (15x)} [20.9 - (xO_{2 Act} / (1 - xH_{2}O))] (1 - xH_{2}O) / 5.9$$

$$= V_{NOx (15x)} [20.9 (1 - xH_{2}O) - xO_{2}) / 5.9$$

$$m_{NOx} = PVM_{NOx} = V_{NOx (15X)}$$
 [20.9 (1 - χH_2O) - χO_2) * P * M_{NOx} / (RT * 5.9)

C

CO and VOC are calculated by correcting for moisture using ideal gas law. Same as NO_x calculation except only moisture correction is used:

$$V_{CO Act} = V_{CO Dry} (1 - \chi H_2 O)$$
 $m_{CO} = PV_{CO Act} M_{CO} / RT$
 $= PV_{CO Dry} (1 - \chi H_2 O) M_{CO} / RT$

pg/J = picograms per joule

SUPPLEMENT C

TO

COMPILATION OF AIR POLLUTANT EMISSION FACTORS

VOLUME I: STATIONARY POINT AND AREA SOURCES

TABLE 1.4-1. UNCONTROLLED EMISSION FACTORS FOR NATURAL GAS COMBUSTIONa

1	Particulate ^b		Sulfur	dioxidec	Mitroge	n oxides ^d	Carbon	onoxide	Volatile organics			
Furnace mize & type (10 ⁶ Btu/hr heat input)									Normethane		Hethane	
	kg/106m3	1b/106 fe3	kg/106m3	1b/10 ⁶ ft ³	kg/106w3	15/106 ft3	kg/106m3	16/10 ⁶ ft ³	kg/106m3	1b/106 ft3	kg/10 ⁶ m ³	1b/106 ft3
Utility boilers (> 100)	16 + 80	1 - 5	9.6	0.6	8800 ^h	550 ^h	640	40	23	1.4	4.8	0.3
Industrial boilers (10 - 100)	16 - 80	1 - 5	9.6	0.6	2240	140	560	35	44	2.8	48	3
Dowestic and commercial boilers (< 10)	16 ~ 80	1 - 5	9.6	0.6	1600	100	320	20	84	5.3	43	2.7

Expressed as weight/volume fuel fired.

bReferences 15-18.

PReferences 15-18.

CReference 4. Based on avg. sulfur content of natural gas, 4600 g/10⁶ Nm³ (2000 gr/10⁶ scf).

dReferences 4-5, 7-8, 11, 14, 18-19, 21.

Expressed as NO₂. Tests indicate about 95 weight X NO_X is NO₂.

fReferences 4, 7-8, 16, 18, 22-25.

SReferences 16, 18. May increase 10 - 100 times with improper operation or maintenance.

Hor tangentially fired units, use 4400 kg/10⁶ m³ (275 1b/10⁶ ft³). At reduced loads, multiply factor by load reduction coefficient in Figure 1.4-1. For potential NO_X reductions by combustion modification, see text. Note that NO_X reduction from these modifications will also occur at reduced load conditions.

UNCONTROLLED EMISSION FACTORS FOR FUEL OIL COMBUSTION TABLE 1.3-1. EMISSION FACTOR RATING: A

		culate ^b	Su] fui	· Dioxide ^C	Sul	fur Trioxide	Ca	rbon Monoxide ^d	Mitrogen	Oxide [®]		Volatile Nonmethan	Organica	f Hethane
Boiler Type	kg/10 ³ 1	15/10 ³ ga1	kg/10 ³ 1	1b/10 ³ gal	kg/10 ³ 1	15/10 ³ g=1	kg/10 ³ 1	15/10 ³ gal	kg/10 ³ 1	1b/10 ³ gal	kg/10 ³ 1	16/10 ³ ga1	kg/10 ³ 1	1b/10 ³ ga1
Utility Boilers Residual Oil		8	195	157 S	0.345 ^h	2.95 ^h	0.6	5 (1	8.0 2.6)(5) ¹	(105)(42) ¹	0.09	0.76	0.03	0.28
Industrial Boilers Residual Oil Distillate Oil	8 0.24	g 2	19S 17S	157S 142S	0.245 0.245	2 \$ 2\$	0.6	5 5	6.6 ^J	55 ^Ĵ 20	0.034 0.024	0.28 0.2	0.12 0.006	1.0 0.052
Commercial Boilers Residual Oil Distillate Oil	\$ 0.24	g. 2	198 175	1575 1425	0.24S 0.24S	25 25	0.6	5	6.6	55 20	0.14	1.13	0.057 0.026	0.475 0.216
Residential Furnace Distillate Off	0.3	2.5	17 S	1425	0.245	25	0.6	5	2.2	18	0.085	0.713	0.214	1.78

Boilers can be approximately classified according to their gross (higher) heat rate as shown below:

Utility (power plant) boilers: >106 x 109 J/hr (>100 x 106 Btu/hr)

Industrial boilers: 10.6 x 109 to 106 x 109 J/hr (10 x 106 to 100 x 106 Btu/hr)

Commercial boilers: 0.5 x 109 to 10.6 x 109 J/hr (0.5 x 106 to 10 x 106 Btu/hr)

Residential furnaces: <0.5 x 109 J/hr (<0.5 x 106 Btu/hr)

References 3-7 and 24-25. Particulate matter is defined in this section as that material collected by EPA Method 5 (front half catch).

References 1-5. 5 indicates that the weight I of sulfur in the oil should be multiplied by the value given.

dReferences 3-5 and 8-10. Carbon monoxide emissions may increase by factors of 10 to 100 if the unit is improperly operated or not well maintained. Expressed as NO2. References 1-5, 8-11, 17 and 26. Test results indicate that at least 95% by weight of NOx is NO for all boiler types except residential furnaces, where about 75% is NO.

References 18-21. Volatile organic compound emissions are generally negligible unless boiler is improperly operated or not well maintained, in which case emissions may increase by several orders of ungnitude.

Sparticulate emission factors for residual oil combustion are, on average, a function of fuel oil grade and sulfur content:

^{1.25(5) + 0.38} kg/103 liter [10(5) + 3 lb/103 gal] where S is the weight % of sulfur in the oil. This relationship is based on 81 individual tests and has a correlation coefficient of 0.65.

Grade 5 oil: 1.25 kg/105 liter (10 1b/103 gal)

Grade 4 oil: 0.88 kg/103 liter (7 1b/103 gal)

hReference 25.

Use 5 kg/103 liters (42 lb/103 gal) for tangentially fired boilers, 12.6 kg/103 liters (105 lb/103 gal) for vertical fired boilers, and 8.0 kg/103 liters (67 lb/10 gal) for all others, at full load and normal (>15%) excess air. Several combustion modifications can be employed for NOx reduction: (1) limited excess air can reduce NO, emissions 5-207. (2) staged combustion 20-407. (3) using low NO, burners 20-507, and (4) ammonia injection can reduce NO, emissions 40-70% but may increase emissions of ammonia. Combinations of these modifications have been employed for further reductions in certain boilers. See Reference 23 for a discussion of these and other NO_X reducing techniques and their operational and environmental impacts.

Nitrogen oxides emissions from residual oil combustion in industrial and commercial boilers are strongly related to fuel nitrogen content, estimated more

accurately by the empirical relationship:

kg NO2/103 liters = 2.75 + 50(N)2 [15 NO2/103gal = 22 + 400(N)2] where N is the weight % of nitrogen in the oil. For residual oils having high (>U.5 weight 1) nitrogen content, use 15 kg NU./103 liter (120 lb NO./103gal) as an emission factor.

United States Environmental Protection Agency Office of Air Quality Planning And Standards Research Triangle Park, NC 27711 EPA-450/2-89-001 April 1989

AIR



ESTIMATING AIR TOXICS EMISSIONS FROM COAL AND OIL COMBUSTION SOURCES

REPRODUCED BY
U.S. DEPARTMENT OF COMMERCE
NATIONAL TECHNICAL
INFORMATION SERVICE
SPRINGFIELD, VA 22161

TABLE 4-1. SUMMARY OF TOXIC POLLUTANT EMISSION FACTORS FOR OIL COMBUSTION

	Emission Factor (1b/10 ¹² Btu)						
Pollutant	Residual Oil	Distillate Oil					
Arsenic	19	4.2					
Beryllium	4.2	2.5					
Cadmium	15.7	10.5					
Chromium	21	48					
Copper	280	280					
Lead	28 ^c	8.9 ^d					
Mercury	3.2	3.0					
Manganese	26	14					
Nickel	1260	170					
POM	8.4 ^b	22.5					
Formaldehyde	405 ^e	. 405 ^e					

^aAll emission factors are uncontrolled, and are applicable to oil-fired boilers and furnaces in all combustion sectors unless otherwise noted.

^bThis value was calculated using all available residual oil data given in Table 4-35. If the upper end of the range of available data is excluded when calculating an average value (which could be used in this table), the average factor for POM from residual oil combustion becomes $4.1 \, 1b/10^{12} \, BTU$.

CApplicable to utility boilers only.

dapplicable to industrial, commercial, and residential boilers.

The formaldehyde factors are based on very limited and relatively old data. Consult Table 4-37 and accompanying discussion for more detailed information.

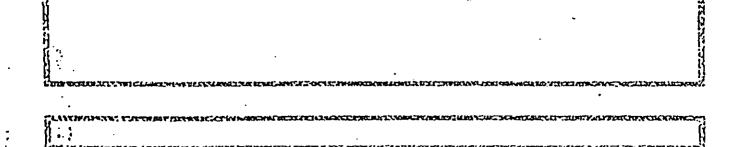
Emissions Assessment of Conventional Stationary Combustion Systems: Volume V: Industrial Combustion Sources

TRW, Inc. Redondo Beach, CA

Prepared for

Industrial Environmental Research Lab. Research Triangle Park, NC

1981



U.S. Gegativest of Commerce
Hational Technical Information Service
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TABLE 61. COMPARISON OF EXISTING TRACE ELEMENT EMISSION FACTOR DATA WITH RESULTS OF CURRENT STUDY OF OIL-FIRED INDUSTRIAL COMBUSTION SOURCES, pg/J

								,
		istillate fired bot			Resident	dual d boilers		
		Existin	ig data		ŗ.	xisting da	ıta	_
Element	Current s tudy	Ref. 42	Ref. 43	Current study	Ref. 42	Ref. 21	Ref: 28	
(1A) munimulA	178	15	250	177	156	87	132	
Arsenic (As)	3.5	1.3	1.5	1.2	9.1	18	12	
Barium (Ba)	1.2	8.4	16	3.3	9.`5	29	31	
Calcium (Ca)	75	845	450	229	780	700	3	
Cadalian (Cd)	1.3	2.5	11	0.66	•		1.9	
Cobalt (Co)	3.6	2.3	1.0	11	•			
Chromium (Cr)	24	36	29	29	·			
Copper (Cu)	37	205	160	10	න	0		_
Fluorine (F)	_	14	_	-	1	07/		V
Iron (Fe)	363	545	140	83	· · · · · · · · · · · · · · · · · · ·			
Hercury (!!g)	-	1.7	1.2	-	:	à =	5	
Potassium (K)	85	60	230	261	2 {	\mathcal{L}		•
Lithium (Li)	0.5	1:5	1.2	1.1	.	4	1.7	
Maunesium (Hg)	• 42	40	210	24	111	297	2384	
Nickel (Ni)	255	112	290	728	804	964	433	
tead (Pb)	24	48	42	2	7	80	34	
Antimony (Sb)	_	1.7	5.7		21	10	25	
Silicon (Si)	735	173		8655	1610	400	595	
Yanadium (V)	195	30	2.9	366	250	3656	714	٠.
Zinc (Za)	42	40	110	33	46	29	66	

UF COGENERATION PROJECT EXAMPLE CALCULATIONS - NATURAL GAS

ROWS listed below correspond to the ROW listed in Table.

Table A-1: (Note: all other data not calculated but supplied by manufacturer)

ROW 13-Heat Input (10⁶BTU/hr):

Power (kw) x Heat Rate (10⁶BTU/kwh)

 $43,262.0 \times 8,043/10^6 = 348.0 \times 10^6 BTU/hr$

ROW 14-Natural Gas (lb/hr):

Heat Input (10⁶BTU/hr) ÷ Fuel Heat Content (BTU/lb)

 $348.0 \times 10^6 \div 19,000 = 18,313.5 \text{ lb/hr}$

Note: 19,000 is input as 0.019 since heat input is in 10⁶BTU, i.e. 348.0

ROW 15--Natural Gas (CF/hr):

Heat input (10⁶BTU/hr) ÷ Heat content (BTU/CF)

 $348.0 \times 10^6 \div 946 = 367,818.5 \text{ CF/hr}$

ROW 21--Volume Flow (acfm) - See Note A in emission factors and calculations:

V = mRT/PM

 $1,036,552 \text{ lb/hr} \times 1,545 \times (785 + 460^{\circ}\text{K}) \div (27.8 \times 2,116.8 \text{ lb/ft}^2) \div 60(\text{min/hr})$ = 564,678 acfm

ROW 22--Volume Flow (scfm) - See Note A:

Same as ROW 21 except adjusted for standard temperature of 68°F

$$1,036,552 \text{ lb/hr} \times 1,545 \times (941 + 68^{\circ}\text{K}) \div (27.8 \times 2,116.8) \div 60$$

= 239,478 scfm

ROW 32-Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$564,678 \text{ (acfm) } x (257 + 460^{\circ}\text{K}) \div (785 \div 460^{\circ}\text{K})$$

= 325,200 acfm

ROW 35--Velocity (ft/sec):

Volume Flow (ft³/min)
$$\div$$
 Area (ft²) \div 60 sec/min
325,200 ft³/min \div 60 \div (10² \div 4 x 3.14159)
= 72.59 ft/sec

Table A-2:

ROWS 59, 64, 69, 75, 81, 118, 156, and 159--(Except Duct Burner):

Emissions in Tons per year; example for particulate:

2.5 lb/hr x 8,760 hrs/yr
$$\div$$
 2,000 lb/ton
= 10.95 ton/yr

For Duct Burner and Oil Firing capacity factors were used. Example for duct burner: $1.87 \text{ lb/hour} \times 0.30 \times 8,760 \div 2,000 = 2.46 \text{ tons per year.}$

ROW 63--SO₂ Emissions (lb/hr):

$$367,818.5 \text{ cf/hr} \times 1 \text{ gr} \div 7,000 \text{ gr/lb} \times 2 \text{ lb } SO_2/\text{lbS} \div 100 \text{ cf}$$

= 2.82 lb/hr

4 ppm x (1-6.1/100) x 564,678 acfm x 2,116.8 lb/ft² x 12 (molecular wgt. of carbon)
x 60 min/hr
$$\div$$
 (1,545 x (785 +460) + 10⁶)
= 1.59 lb/hr

Table A-3:

Emission factors for oil presented in Table 4-1 of EPA (1989) multiplied by heat input; example for arsenic: 382.6×10^6 Btu/hour x $4.216/10^{12}$ Btu = 0.0016 lb/hour

ROW 117--H₂SO₄ Mist Emission (lb/hr):

Based on 5 percent SO₂ converted to acid mist

1.05 lb
$$SO_2/hr \times 0.05 \times 98 \div 64$$
 (or a ratio 3.06/2)
= 8.04 x 10^2

Table A-4:

Emission factor multiplied by heat input

U.S. DEPARTMENT OF COMMERCE National Technical Information Service PB-296 390

Emission Assessment of Conventional Stationary Combustion Systems; Volume II Internal Combustion Sources

TRW, Inc., Redondo Beach, CA

Prepared for

Industrial Environmental Research Lab, Research Triangle Park, NC

Feb 1979

TABLE 52. COMPARISON OF TRACE ELEMENT EMISSION FACTORS FOR DISTILLATE OIL-FUELED GAS TURBINES AND DISTILLATE OIL ENGINES

<u>.</u>		Mean Emission	Factor, pg/J
1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	Trace Element	Distillate Oil Fueled Gas Turbine	Distillate Oil Reciprocating Engine
i Vi	Aluminum	64	66
}	Antimony	9-4	12
	Arsenic	2.1	2.2
ž. 1:	Barium	. 8.4	14 ·
	Beryllium	0.14	0.03
٠.٠. . ۲۲ ع	Boron	28	11
	Bromine	1.8	4.0
STAIL ROTA	Cadmium	1.8	3.1
	Calcium	330	237
(°)-	Chromium	20	26
ž	Cobalt	3.9	5.7
	Copper	578	453
	Iron	256	325
	Lead	25	26
	Magnesium	100	44
ξ	Manganese	145	16
, , ,	Mercury	0.39	0.13
	Molybdenum	3.6	12.5
Υ. 	Nickel	526 .	564
	Phosphorus	127	97
	Potassium	185	179
	Selenium	2.3	2.1
	Silicon	575 1	301
	Sodium	590	1625
3	Tin	35	9.1
<u>}</u> .	Vanadium ·	1.9	0.95
-	Zinc	294	178

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Toxic Air Pollutant Emission Factors—A Compilation For Selected Air Toxic Compounds And Sources

By
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Patricia A. Cruse
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U.S. ENVIRONMENTAL PROTECTION AGENCY Office Of Air And Radiation Office Of Air Quality Planning And Standards Research Triangle Park, North Carolina 27711

October 1988

INDUSTRIAL PROCESS	\$1C CODE	ERISSION SOURCE	scc	POLLUTANT	CAS HUBER	ERISSION FACTOR	HOTES	REFERENCE
Oil combustion		Scotch marine boilers, distillate oil	10300501	POH		17.7 pg/J	Uncontrolled	114
OIL combustion		East iron sectional boilers, distillate oil	10300501	POR		<14.9 pg/J	Uncontrolled, home heating application	114
Oil compustion		Not air furnece, distillate oil	10300501	POR		<0.14 pg/J	Uncontrolled, same reference also lists <15.4 for same boiler/fuel type	114
0il combustion	49	Boiler flue gas	1	Tetrachlorodibenzo-p-diox in, 2,3,7,8-	1746016	Not detectable	tow ash, 2% sulfur oil, sampled after heat each., before ESP, 2378-1CDD detec, limit=<4.2-<7.9 ng/m3	119
Oil combustion	49	flue gas	1	Tetrachlorodibenzofuran, 2,3,7,8-	5120 <i>7</i> 319	Not detectable	iow ash, ZX sulfur oil, sampled after heat exch., before ESP, 2378-TCDD detec. limit=40.67-<1.3ng/m3	119
Oil combustion, commercial		Residual oil-fired tangential furnaces	103004	Vanadius	7440622	3660 pg/J	Uncontrolled, based on reported emissions and angineering judgement	54
Oil compustion, commercial	•	tesidual all-fired wall furnaces	103004	Yenedius	7440622	3660 pg/1	Uncontrolled, based on reported emissions and angineering judgment	54
Oil combustion, commercial		Tangential furnace, residual mil	103004	Selmius	7782492	10.1 pg/2	Uncontrolled, based on reported emissions data and engineering judgement	54
Oil combustion, commercial		Wall furnace, residual oil	103004	Selenium	7762492	10.1 pg/ <i>1</i>	Uncontrolled, based on reported emissions data and engineering judgement	54
Oil compustion, commercial		Scotch marine boilers, residual oil	10300401	POH		0.95 pg/J heat input	. Uncontrolled, represents benze(s)pyrene only	114
Oil combustion, commercial	į.	Distitlate oil-fired tangential furnaces	103005	Yanadiya	7440622	30.0 pg/J	Uncontrolled, based on reported emissions data and engineering judgement	54
Oil combustion, commercial		Distillate oil fired wall furnaces	103005	Variation	7440622	30.0 pg//	Uncontrolled, based on reported emissions data and engineering judgement	54
Oil compustion, commercial	•	Tangential durnace, distillate oil	103005	Selenium	7782492.	10.1 pg/1	Uncontrolled, based on reported emissions data and engineering judgement	54



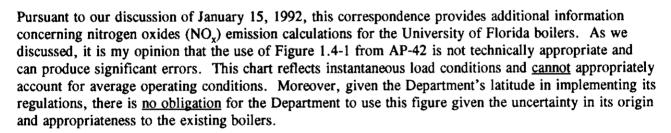
January 30, 1992

Mr. C. H. Fancy, P.E., Chief Bureau of Air Regulation Florida Department of Environmental Regulation Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Alachua County--A.P. RE: UF Cogeneration Project AC 01-204652

Attention: John Reynolds

Dear Mr. Fancy:



RECEIVED

Resources Managenient

Presented in Table 1 is the average fuel usage for Units 3 and 5 for 1988, 1989, and 1990. The average load factor on gas can be calculated directly using fuel usage and hours of operation data presented in the annual operation report. The maximum fuel usage at 100 percent load is specified as cubic feet per hour for each boiler in Specific Condition 1 of each permit. The effective full load operation can be calculated by dividing the total fuel usage by the potential full load fuel usage. The equivalent full load operating hours can be used to calculate average load using the actual operating hours given in the annual operating reports. Adjustments of oil usage are made by subtracting the hours used on oil from the total hours. This calculation is somewhat uncertain since the load factor for oil is also unknown.

The load factors for natural gas presented in Table 1 are different than those calculated and presented in the Department's December 31, 1991 letter. The difference in calculating load factors using two independent methods are as high as about 25 percent. This is one source of error that can be introduced.

Another source of error is using the load coefficients as a means of calculating an average weighted emission factor. Table 2 presents this comparison. This table presents the load reduction coefficient and emission factor as a function of load (taken from Figure 1.4-1). The table also presents some possible operating conditions in terms of the percent of operation at a specific load. For example, if 50 percent

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KBN ENGINEERING AND APPLIED SCIENCES, INC.



of the time the boiler operated at 100 percent load and 50 percent of the time it operated at 40 percent load then the average weighted load when operating would be 70 percent. The average weighted emission factor can then be calculated by using the specific emission factors for each load. The table also lists the emission factor obtained directly from Figure 1.4-1 using the average weighted load. This example calculation clearly indicates that the appropriate emission factor would be 20 percent higher than an emission factor calculated using an average load. Table 2 presents other examples that clearly indicate an error introduced by using Figure 1.4-1. Since there are no available data to determine the various instantaneous load conditions during the year, the use of Figure 1.4-1 is not technically appropriate. Indeed, all operating reports submitted for natural gas firing from electric utilities over the last 10 years use the emission factor in Table 1.4-1.

The errors introduced when calculating the average load factor and when calculating the average weighted emission factor clearly suggest that using Figure 1.4-1 is inappropriate. There are several other factors that should also be considered.

The Department should also be aware that under Rule 17-2.100(3)(b) Florida Administrative Code, allowable emissions can be specified as actual emissions as long as the limits are federally enforceable. Current interpretation suggests that the existing limits are federally enforceable, since the units in question (Units 3 and 5) have received BACT determinations.

Table 3 presents comparison of potential and requested emissions of NO_x for various scenarios. The permit application requested a 94 percent reduction in potential NO_x emissions from the existing boilers. The request was based on obtaining sufficient emission reductions from the existing units to eliminate the need for PSD review of NO_x. With this strategy the requested potential emissions of NO_x, including the CT/duct burner and limited operation of existing Units 4 and 5, are 298.37 tons per year. This is a decrease in potential emissions of over 800 tons per year or 278 percent. Without this strategy of taking NO_x reductions from Units 4 and 5, there is no need to take any operating limits for Units 4 and 5. Under this scenario, the potential NO_x emissions from Units 4 and 5 are 502 tons per year or 7.8 times higher than originally requested for these units. Clearly the operating limitations proposed in the permit have significant environmental advantages over other scenarios.

Your consideration in this matter is appreciated. Please call if you have any questions.

Sincerely,

Kennard F. Kosky, P.E.

Robert C. Mclaun &

President

KFK/tyf

cc: Scott Osbourn

9. Reynolds
6. Holladay - Dist
9. Harper, 5-74
91062A115
0. Shawer, NPS

Table 1. UF Heating Plant Fuel Use, Hours of Operation and Average Calculated Load Factor

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Unit	Year	Fuel Use		Operation	at Full Load	Actual	Load
	iear	Gas (Mcf)	Oil (gal)	Gas (hrs)	Oil (hrs)	Hours	Factor Gas/Oil
Unit 3	1988	464,100	26,268	3,033.3	24.6	4,451.6	68.77%
	1989	392,375	11,269	2,564.5	10.6	5,057.2	50.89%
	1990	248,350	19	1,623.2	0.0	2,648.1	61.30%
	Avg.	368,275	12,519	2,407.0	11.7	4,052.3	59.69%
Unit 5	1988	537,506	537,506	3,277.5	503.9	6,411.0	58.83%
	1989	403,205	28,481	2,458.6	26.7	4,549.9	54. 5 7%
	1990	416,485	5,557	2,539.5	5.2	5,115.6	49.73%
	Avg.	452,399	190,515	2,758.5	178.6	5,358.8	54.50%

Table 2. Calculated Emission Factors Under Possible Operating Conditions

Load	Load Reduction Coefficient	Emission Factor (1b/mmcf)	Percent at Load	Percent at Load	Percent at Load	Percent at Load	Percen at Loa
100%	1.00	550	50%		65 x	75%	
95%	0.90	495					70 2
90x	0.81	446		70%			
85%	0.74	407					
80%	0.67	369					
75%	0.60	330					
70%	0,55	303					
65%	0.51	281					
60%	0.48	264					
55X	0.43	237					
50X	0.40	220					
45%	0.37	204					
40%	0.35	193	50%				
35%	??	188					
30%	??	180			35 x		
25%	??	172					
20%	??	164					
15%	??	156					
10%	??	148		30%			
5%	??	140				251	30%
	Average	Load =	70%	66 %	76%	76 %	681
٨v	erage Emission Fa	actor =	371	356	421	448	389
Fi	gure 1.4-1 Factor	c =	303	285	338	338	294
Di	fference =		20%	221	221	28%	281

Table 3. Comparison of Existing and Proposed Potential Emissions for the UF Cogeneration Project

		•		
Unit	Potential Emissions (tons/year)	Emissions	Emission Reduction (tons/year)	Decrease
1	128.4	0.0	(128.4)	100%
2	128.4	0.0	(128.4)	100%
3	368.6	0.0	(368.6)	100%
4	107.0	5.5	(101.5)	95%
5	395.1	59.0	(336.1)	85%
Total:	1,127.5	64.5	(1,063.0)	94%
Cogen Only	233.9	233.9	NA	NA
w/Cogen and 4&5 Reduction		298.4	(829.1)	278%
w/Cogen and No 4&5 Reduc	736.0		(327.0)	44%
Emissions In (without red in Units 4&	ductions)	437.6 1472	tons/year	

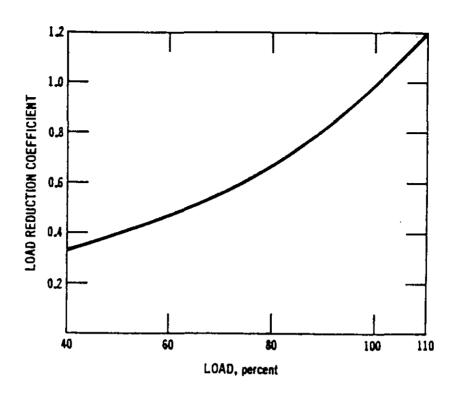


Figure 1.4-1. Load reduction coefficient as function of boiler load. (Used to determine $NO_{\mathbf{X}}$ reductions at reduced loads in large boilers.)

References for Section 1.4

- 1. D. M. Hugh, et al., Exhaust Gases from Combustion and Industrial Processes, EPA Contract No. EHSD 71-36, Engineering Science, Inc., Washington, DC, October 2, 1971.
- J. H. Perry (ed.), <u>Chemical Engineer's Handbook</u>, 4th Edition, McGraw-Hill, New York, NY, 1963.
- 3. H. H. Hovey, et al., The Development of Air Contaminant Emission Tables for Non-process Emissions, New York State Department of Health, Albany, NY, 1965.
- 4. W. Bartok, et al., Systematic Field Study of NO_x Emission Control Methods for Utility Boilers, APTD-1163, U. S. Environmental Protection Agency, Research Triangle Park, NC, December 1971.

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Florida Department of Environmental Regulation

Twin Towers Office Bldg. ● 2600 Blair Stone Road ● Tallahassee, Florida 32399-2400 Lawton Chiles, Governor

Carol M. Browner, Secretary

January 16, 1992

Mr. Greg Worley Air Enforcement Branch EPA Region IV 345 Courtland Street NE Atlanta, Georgia 30365

Re: Permit Application AC 01-204652, PSD-FL-181 University of Florida Cogeneration Project

Dear Mr. Worley:

EPA's quidance is needed to resolve an issue with the above PSD permit application. A copy of the application was forwarded to EPA last November. The issue is whether or not to allow emission offset credits for Boilers 3 and 5 as if they had been run at full load. Data from the operation reports show that the boilers did not run at full load during the years in question.

The applicant wants us to disregard the emission factor adjustment called for in AP-42, Figure 1.4-1, for Boilers 3 and 5 so they can escape PSD review for NOx. They want us to use the discretion provided for in Florida Administrative Code, Rule 17-2.100(3)(b), to presume that their actual boiler emissions were equal to the allowable emissions which were based on full load operation.

We were advised by Ron Ryan, OAQPS, that the AP-42, Table 1.4-1 emission factor should not be applied without adjustment for load according to Figure 1.4-1. The applicant argues that Figure 1.4-1 should apply only to instantaneous determinations and should not be used where long term averaging is involved.

Any input EPA may provide will be appreciated. If more clarification is needed, please contact John Reynolds of our staff at 904-488-1344.

Sincerely,

C. H. Fancy, P.E.

Chief

Bureau of Air Regulation

CHF/JR/plm





Florida Department of Environmental Regulation

Twin Towers Office Bldg. ● 2600 Blair Stone Road ● Tallahassee, Florida 32399-2400 Lawton Chiles, Governor

Carol M. Browner, Secretary

January 9, 1992

CERTIFIED MAIL - RETURN RECEIPT REQUESTED

Mr. R. W. Neiser Senior Vice President-Legal and Gov. Affairs Florida Power Corporation 3201-34th Street South St. Petersburg, Florida 33733

Dear Mr. Neiser:

Permit Application AC 01-204652, PSD-FL-181

The Department received Florida Power Corporation's letter dated January 2, 1992, and considers it a partial response to one issue in the Department's incompleteness letter of December 31, 1991. The additional information requested below applies only to this one issue concerning NO_X emission factors.

In the absence of NO_X emission test data for the years in question, please provide the following data for Boilers Nos. 3 and 5 at the University of Florida facility:

- Boiler and burner manufacturer, address and phone number.
- Date boilers were manufactured and date installed.
- Boiler and burner type/configuration (provide sketch).
- Design maximum heat input rate.
- Full description and dates of all burner modifications, if any.

If clarification is needed on any of the above, please contact the permit engineer, John Reynolds, at (904) 488-1344.

Sincerely,

C. H. Fancy, P.E.

Chief

Bureau of Air Regulation

CHF/JR/plm

S. Osbourn, FPC

K. Kosky, P.E., KBN

.A. Kutyna, NED (w/Jan. 2 ltr)

J. Harper, EPA ("

C. Shaver, NPS ("

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٥	Permit: AC 01-2	04652
S	PSD-FL-	181
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3. Article Addressed to:	4a. Article Number .
Mr. R. W. Neiser Senior Vice President-Legal and Gov. Affairs Florida Power Corporation 3201 - 34th Snreet South St. Petersburg, FL 33733	P 832 538 764 4b. Service Type Registered Insured Cod Express Mail Return Receipt for Merchandise 7. Date of Delivery AN 16 1992
5. Signature (Addressee) 6. Signature (Agent)	Addressee's Address (Only if requested and fee is paid)
PS Form 3811, October 1990 #U.S. GPO: 1990-273-	861 DOMESTIC RETURN RECEIPT



Office of Air Quality Planning and Standards Research Triangle Park, North Carolina 277715 CE/VEO UNITED STATES ENVIRONMENTAL PROTECTION AGENCY

Mr. John Reynolds
Florida Department of Environmental Regulativen Division of Air
Stone Road

The Stone Road

Dear Mr. Reynolds:

To confirm our telephone conversation of January 8, 1992 regarding NO, emissions estimates for natural gas fired boilers, the load reduction coefficient determined from Figure 1.4-1 of AP-42 should be used in conjunction with the utility boiler factors in Table 1.4-1 to estimate emissions accurately. addition, the estimates will be more accurate if the load percent used represents a fairly constant level, rather than an average of a widely varying load level. Thus, if estimates were made for several representative periods with different loads and summed the result should be more accurate than using a single average load for the entire period. Removing the hours that the boiler was not operating from the averaging period is the first and probably the largest improvement that could be made to the estimate's accuracy.

I could not find a detailed derivation of Figure 1.4-1 in our background documentation files, although it appears that references 7 and 14 of AP-42 section 1.4 contain a large amount of relevant data. Please call if I can be of further assistance.

Sincerely,

Ronald Ryan

Rouald Pyan

Environmental Engineer

Emission Factors and Methodologies Section



Florida Department of Environmental Regulation

Northeast District • Suite B200, 7825 Baymeadows Way • Jacksonville, Fiorida 32256-7577

Lawton Chiles, Governor

Carol M. Browner, Secretary

January 7, 1992

Mr. Scott Osborn Florida Power Corporation Post Office Box 14042 St. Petersburg, Florida 33733

> Alachua County - AP Florida Power Corporation Cogen Project at U of Fl.

Dear Mr. Osborn:

The applications for transfer of permits enclosed are being returned per the January 06 (Patty Adams and Johnny Cole) teleconference.

The \$250.00 for the transfer fees is to be refunded under separate cover.

The cogen certificate is to address the transfer of permits issue.

If there are any questions, please contact Johnny Cole at the letterhead address/telephone number.

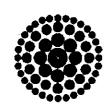
Sincerely,

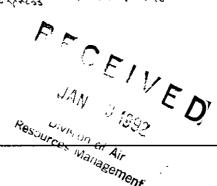
Andrew G. Kutyna, P.: District Air Program Administrator

AGK:JC:bt

cc: Patty Adams, DARM, BAR

Department of Environmental Regulation Routing and Transmittal Slip To: (Name, Office, Location) Remarks: Date From: air/Jax Phone





Florida Power

January 2, 1992

Mr. Barry Andrews
Bureau of Air Regulation
Florida Department of Environmental Regulation
Twin Towers Office Building
2600 Blair Stone Rd.
Tallahassee, Florida 32399-2400

Dear Barry:

Re: University of Florida Cogeneration Project.

This letter is in response to questions by your staff regarding the proper application of the NO_x emission factor for natural gas-firing of external combustion sources (AP-42 Section 1.4). Table 1.4-1 presents a NO_x emission factor for utility boilers of 550 lb/10⁶ ft³ of natural gas fired. A footnote to this factor directs the user to "multiply the factor by the load reduction coefficient in Figure 1.4-1 at reduced loads."

As I am the author of the current AP-42 section, I am compelled to submit additional information for your consideration regarding the intent of Figure 1.4-1 within the context of this section. Section 1.4 was originally published in 1973 and included Figure 1.4-1. At that time, no reference was supplied for the figure. When I revised the section in 1982 (the current version is dated October 1986 and reflects some minor editorial changes made to the 1982 version), the figure was retained, although no reference could be identified. The rationale was that the figure may prove helpful for more accurately estimating an instantaneous or short-term emissions rate -- where the load (in percent) required for application of this figure may be readily available. You will note that the figure does not cite application of a "load factor" or a "capacity factor", rather an instantaneous representative load, in percent.

The AP-42 document is a compilation of emission factors, which are average values derived by averaging available data of acceptable quality. These factors are routinely applied in

many contexts (e.g., to estimate the collective emissions from a number of sources, as in emission inventories; to predict emissions from new or proposed sources; to obtain annual or short-term emission estimates; etc.) and the document emphasizes that care should be taken to apply each factor in a manner consistent with its intended use.

To help users understand the reliability and accuracy of AP-42 emission factors, each factor is assigned a rating (A through E, with A being the best) which reflects the quality and the amount of data on which the factors are based. In general, factors based on many observations or on more widely accepted test procedures are assigned higher rankings. For instance, an emission factor based on 10 or more source tests on different plants would likely get an A rating, if all tests were conducted using a single valid reference measurement method or equivalent techniques (AP-42, Introduction, p.2). All NO_x emission factors in Section 1.4 have been assigned A ratings.

Given this background, it is my belief that in calculating annual NO_x emissions estimates from a natural gas-fired utility boiler, it is appropriate to apply only the factor provided in Table 1.4-1. Precedent has been set for such an interpretation in numerous applications, some of which have been reviewed by your staff. However, in order to confirm the appropriateness of the use of Figure 1.4-1, I have had discussions with Mr. Ron Ryan of the Emission Factor and Methodologies Section, Emission Inventory Branch, of the Office of Air Quality Planning and Standards. (Mr. Ryan may be contacted at (919) 541-4330.) Mr. Ryan stated that the origin and proper application of Figure 1.4-1 were, at best, unclear. He added that it might be best to apply such a figure to short-term emission estimates only, and contends that such an interpretation is supported by the practical difficulty of obtaining a representative "load" to apply to an annual emission estimate.

If you should have any questions, or wish to meet to discuss this issue in more detail, please do not hesitate to contact me at (813) 866-5158.

Sincerely,

Scott H. Osbourn Environmental Engineer

cc: Preston Lewis, FDER Ron Ryan, OAQPS

John Reynolds

Clew Holladay

Jowell Harper, ECA

Chair Shower, Mis

Chair Sallins ED



Florida Department of Environmental Regulation

Twin Towers Office Bldg. • 2600 Blair Stone Road • Tallahassee, Florida 32399-2400 Lawton Chiles, Governor Carol M. Browner, Secretary

December 31, 1991

CERTIFIED MAIL - RETURN RECEIPT REQUESTED

Mr. R. W. Neiser Senior Vice President-Legal and Gov. Affairs Florida Power Corporation 3201-34th Street South St. Petersburg, Florida 33733

Dear Mr. Neiser:

Re: Permit Application AC 01-204652 UF Cogeneration Project

The subject application and permit fees for the UF cogeneration facility were received by this office on December 2, 1991, after a pre-application meeting on November 13 with FPC staff. About two weeks later FPC staff contacted us to inquire about the status of the application. They emphasized the urgency of the project. We indicated to them that our review had not been completed but that we hoped an incompleteness letter might be avoided. Several days later we discovered that PSD applicability for one of the major pollutants (NO_X) was determined incorrectly in the application. We notified your staff and consultants of this by phone on December 19. In order to complete the application, the following additional information and revisions are required:

1. The AP-42 $\rm NO_X$ emission factor for fully loaded natural gas-fired boilers over 100 MMBtu/hr is 550 lbs. $\rm NO_X/MM$ ft³ of fuel fired. For loads less than 100%, the emission factor is reduced according to AP-42, Figure 1.4-1. The 100% factor was used to calculate offset credits of 195.1 tons/yr of $\rm NO_X$ emissions, thus arriving at a net $\rm NO_X$ increase of 38.8 tons/yr. This level of net emissions (less than 40 tons/yr) would preclude PSD review for $\rm NO_X$ as stated in the application. However, analysis of load factors for UF's boilers Nos. 3 and 5 (capacity over 100 MMBtu/hr) during the three year period '88 - '90 reveals the following:

Fuel MM ft^3 per yr./Operating hrs per yr.

				/90
No.	3	464.1/4451.6	392.4/5057.2	248.4/2648.1
No.	5	537.8/6411	403.2/4549.9	416.8/5115.6

Dividing the fuel rates by the operating hours gives the following (assume approximately 1,000 Btu required per pound of steam and 946 Btu per ft³):

Avg. ft^3/hr . (000) / Avg. lbs. Steam per hr. (000)

			/89	/90
No.	3	104.3/98.7	77.6/73.4	93.8/88.7
No.	5	83.9/79.4	88.6/83.8	81.5/77.1

Average load factors are obtained by dividing the steam production by the maximum capacity of 120,000 lbs/hr. The load reduction coefficient is then obtained from AP-42, Figure 1.4-1:

Avg. % Load/Load Reduction Coefficient

			<u>′89</u>	/90
No.	3	82/.65	61/.47	74/.60
No.	5	66/.50	70/.55	64/.49

 ${\rm NO_X}$ emission factors are then obtained by multiplying the load reduction coefficients by the 100% load factor, i.e. 550:

NO_X Emission Factor (lbs/MM ft³ fuel)

No. 3	358	259	330
No. 5	275	303	270

A weighted average emission factor for the 3 yr. period can be based on relative operating hours as follows:

Fraction of Total hrs/Emission Factor

	<u>'88</u>		′ 90	<u>Total</u>
No. 3	.37/132.5	.42/108.8	.21/69.3	310.6
No. 5	.40/110	.28/84.8	.32/86.4	281.2

Thus the NO_X emission credits would be approximately 155 tons/yr instead of the 195.1 tons/yr claimed, resulting in a net increase of about 79 tons/yr instead of 38.8 tons/yr. Due to the above, the application will have to be revised to include PSD review for NOx.

- 2. References in the application to the proposed facility being major on the basis of emissions exceeding 250 tons per year should be changed to 100 tons per year since the HRSG is on the "List of 28" major source categories (fossil fuel boiler exceeding 250 MMBtu/hr input including GT exhaust).
- 3. Page 2 of Form 1.202(1), Item C., implies "low NO_X combustors" are being proposed which is not the case. The revised application should explain that $Low-NO_X$ combustors are not currently available for this model turbine but may be within 5 years. The revision should explain what is required in the initial design to provide for future installation of $Low-NO_X$ burners.
- 4. Emission calculations are not adequately shown in Appendix A. All calculations affecting emissions should be shown in their entirety. For example, the Appendix "A" calculation for the NSPS NO_X emission limit of 75 ppm corrected to 15 percent oxygen is not carried to completion. The set-up is shown, but not the final calculation. The application should clearly show how all emission-related quantities were obtained.
- 5. Total steam production should be shown in Table 1-1 along with design capacity of the HRSG.
- 6. Please evaluate the impact of this project on the following Class I areas: Chassahowitzka National Wilderness Area in Florida and Okefenokee National Wilderness Area in Georgia. This evaluation should include a cumulative PM₁₀ and NO_X Class I increment analysis. An expanded air quality related values analysis (AQRV) should be done since there are no significant impact levels for this analysis. The AQRV analysis includes impacts to soils, vegetation and wildlife.
- 7. Please explain the use of terrain elevations at receptor points in the modeling and show how the elevations input into the model were derived.

Mr. R. W. Neiser Page 4 of 4

If further clarification is needed on any of the above, please contact John Reynolds or Cleve Holladay at (904) 488-1344.

Sincerely,

C. H. Fancy, P.E.

Chief

Bureau of Air Regulation

CHF/JR/plm

A. Kutyna, NED

K. Kosky, P.E., KBN
D. Jones, P.E., FPC

J. Harper, EPA

C. Shaver, NPS

Reading File
John Reynolds 3 12/3/191 PBM
Clive Holladay

P 838 538 758

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PS Form 3811, October 1990 #U.S. GPO: 1990-273-	861 DOMESTIC RETURN RECEIP

1 to 1877



December 2, 1991

Mr. C. H. Fancy, P.E., Chief Bureau of Air Regulation Florida Department of Environmental Regulation Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Subject:

Alachua County - A.P.

University of Florida Cogeneration Project

Dear Clair:

This correspondence presents information discussed during the November 13, 1991 meeting concerning the above referenced project. As stated at the meeting, a three year period was used to calculate actual emissions for the existing University of Florida Heating Plant. Three years were used since the calendar year 1990 was abnormally warm compared with historical data. A quantitative measure of this is reflected by the number of heating degree days observed by the National Weather Service for Gainesville. In 1990, the heating degree days were 709 compared to a historical average of 1,259. The average heating degree days for 1990 and 1989 was 974 which would normally be considered the two year period identified in the Department's rules [Rule 17-2.100(3)(a)] as applicable for calculating actual emissions. However, this period was not representative of actual emissions. Therefore, a three year average of 1988 through 1990 was used to calculate actual emissions. The heating degree days for this period is 1,104 which is more representative of the operation of the UF heating plant.

RECE LEG TO BE DIVISION OF ALL MANAGEMENT.

As stated at the meeting, the use of a combined cycle configuration for the project will considerably reduce emissions through the use of an efficient combustion turbines and waste heat utilization. Over the twenty year life of the project, an average equivalent of about 374,110 barrels of oil will be saved by the project. The reduction in potential emissions by not using oil will be 107 tons per year (TPY) of PM10, 1,850 TPY of SO₂ and 432 TPY of NOx. In addition, the project will save the University of Florida an average of \$5,244,00 per year over 20 years. Indeed, the environmental and economic benefits of the project make it highly advantageous.



Because of the need to proceed expeditiously with this project (i.e., construction start of February 1, 1991), your staff's expeditious review would be greatly appreciated. Please call if you have any questions.

Sincerely, Germond J. Justry

Kennard F. Kosky, P.E.

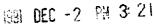
President

cc: Scott Osbourn

W.W. Vierday

Project File

9. Reynolds C. Hisladay G. Cole, NE Dist 9. Harper EPA C. Shareir, 18PS BA/PL





Florida Power

November 25, 1991

Mr. Clair Fancy
Bureau of Air Regulation
Florida Department of Environmental
Regulation
2600 Blair Stone Road
Tallahassee, FL 32399-2400

Dear Mr. Fancy:

Re: University of Florida Cogeneration Project

With regard to our Scott Osbourn and your Patty Adams conversation on November 19, 1991, this is to supplement our filing on November 12, 1991. Enclosed are the original and four copies each of applications for transfer of permit for boilers Nos. 1, 2, 3, 4 & 5 at the Central Heat Plant, University of Florida. Also enclosed is a check in the amount of \$2,750.00 which covers the \$250.00 application fee for the transfer permits and the additional \$2,500.00 to supplement the previous \$5,000.00 check for the air construction permit.

On November 12, 1991, Florida Power Corporation submitted an application to construct a 43-megawatt (MW) cogeneration facility at the existing University of Florida (UF) Central Heat Plant. The proposed cogeneration facility will consist of a combustion turbine (CT) with a generating capability of 43 MW. The steam generated by heat recovery steam generators (HRSGs) will be used for injection into the turbine for emission control and exported to the UF thermal distribution system. One hundred percent of UF's steam requirements will be supplied by the cogeneration plant with existing UF boilers #4 & #5 utilized for back-up capacity.

Mr. Clair Fancy November 25, 1991 Page 2

Upon commercial operation of the cogeneration plant, FPC will be responsible for the operation and common control of the University Heat Plant #2 boilers. Boilers #1, #2, & #3 will be retired in place. Boilers #4 & #5 will be operated as back-up capacity as further documented in these applications. Ownership of all these boilers will remain with the University of Florida.

If you have any questions during the review process, please contact me at (813) 866-4511.

Sincerely.

W. W. Vierday, Manager

Environmental Programs-Licensing

Enclosures

9. Reynolds C. Holladay 9. Cole, NE Dist (WITO requests for AO permits) BA/PL pag/WWV6.Fancy2.Let

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FLORIDA DEPARTMENT OF ENVIRONMENTAL REGULATION 2600 BLAIR STONE RD TALLAHASSEE FL 3239

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KEM Donald

November 25, 1991

Mr. Clair Fancy
Bureau of Air Regulation
Florida Department of Environmental
Regulation
2600 Blair Stone Road
Tallahassee, FL 32399-2400

OF

Dear Mr. Fancy:

Re: University of Florida Cogeneration Project

With regard to our Scott Osbourn and your Patty Adams conversation on November 19, 1991, this is to supplement our filing on November 12, 1991. Enclosed are the original and four copies each of applications for transfer of permit for boilers Nos. 1, 2, 3, 4 & 5 at the Central Heat Plant, University of Florida. Also enclosed is a check in the amount of \$2,750.00 which covers the \$250.00 application fee for the transfer permits and the additional \$2,500.00 to supplement the previous \$5,000.00 check for the air construction permit.

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Florida Department of Environmental Regulation

Twin Towers Office Bldg. • 2600 Blair Stone Road • Tallahassee, Florida 32399-2400 Lawton Chiles, Governor Carol M. Browner, Secretary

November 15, 1991

Mrs. Christine Shaver, Chief Permit Review & Technical Support Branch National Park Service-Air Quality Division Post Office Box 25287 Denver, Colorado 80225

Dear Mrs. Shaver:

Re: Florida Power Corporation

University of Fla. Cogeneration Project

PSD-FL-181

Enclosed for your review and comment is the above referenced PSD permit application. If you have any comments or questions, please contact John Reynolds or Cleve Holladay at the above address or at (904)488-1344.

Sincerely,

Patricia G. Adams

Planner

Bureau of Air Regulation

tricia G. adams

PA/kt

enclosure



Florida Department of Environmental Regulation

Twin Towers Office Bldg. ● 2600 Blair Stone Road ● Tallahassee, Florida 32399-2400 nton Chiles, Governor

Carol M. Browner, Secretary

November 15, 1991

Ms. Jewell Harper, Chief Air Enforcement Branch U.S. EPA - Region IV 345 Courtland Street, NE Atlanta, Georgia 30308

Dear Ms. Harper:

Florida Power Corporation

University of Fla. Cogeneration Project

PSD-FL-181

Enclosed for your review and comment is the above referenced PSD permit application. If you have any comments or questions, please contact John Reynolds or Cleve Holladay at the above address or at (904)488-1344.

> Sincerely, Patricia G. adams

Patricia G. Adams

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PA/kt

enclosure