JAN 06 2002

TEST REPORT On STACK EMISSIONS

BUREAU OF AIR REGULATION

BLEACH PLANT WET SCRUBBER OUTLET

In service at

GEORGIA-PACIFIC PALATKA OPERATIONS

Located in PALATKA, PUTNAM COUNTY, FLORIDA

Prepared for

GEORGIA-PACIFIC CORPORATION

Test Completion Date: October 28th, 2002 Report Submittal Date: November 8th, 2002

Cubix Project No. 7382-FL1

Prepared by



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INTRODUCTION

Emission testing was conducted on a Bleach Plant wet scrubber at the Georgia-Pacific Corporation (GaPac) Palatka Operations facility located on County Road 216 in Palatka, Putnam County, Florida. Carbon monoxide (CO) and other combustion products were measured in the outlet of the scrubber stack. Cubix Corporation, Southeast Regional Office conducted these tests on October 28th, 2002.

The purpose of this testing was to determine the CO emission rates of the scrubber while bleaching softwood in lieu of hardwood as an engineering study. Three one-hour test runs were conducted on the unit documenting process operating data, emission concentrations, and mass emission rates.

The tests followed the principles of the procedures set forth in the <u>Code of Federal Regulations</u>, Title 40, Part 60, Appendix A, Methods 1, 2, 3a, 4, and 10. Table 1 summarizes the background information pertinent to these tests.

This report has been reviewed and is approved for submittal by the following representative:

Cubix Compration

TABLE 1 Background Data

Source Owner:

Georgia-Pacific Corporation

County Road 216 Palatka, Florida 32177 Attention: Joe E. Taylor (386) 329-0027 Phone (386) 328-0014 Facsimile

Email: JETAYLOR@GAPAC.com

Test Contractor:

Cubix Corporation, SE Regional Office

3709 SW 42nd Avenue, Suite 2 Gainesville, Florida 32608

Attention: Roger Osier, Project Foreman

(352) 378-0332 Phone (352) 378-0354 Facsimile Email: rosier@cubixcorp.com

Process Description:

This pulp and paper mill produces both natural and bleached Kraft paper grades. Wood pulp is processed at the Bleach Plant in the manufacture of bleached paper products. The process utilizes chlorine dioxide (ClO₂) for the bleaching of pulp. Emissions from all stages of the bleaching process

are sent to an alkaline wet scrubber.

Test Date(s):

October 28th, 2002.

Location:

Georgia-Pacific Palatka Operations is located on County Road 216 in Palatka, Putnam County,

Florida.

Emission Sampling Point:

The Bleach Plant scrubber (outlet) stack has two 3" diameter flanged NPT sample ports located 90° to each other in the vertical stack before venting to atmosphere, see Appendix A for stack diagram.

Test Participants:

Georgia-Pacific Corporation
Joe Taylor. Test Coordinator

Test Participants (continued):

Cubix Corporation

Roger Paul Osier, Project Foreman James Hastings, Field Technician

Test Methods:

Environmental Protection Agency (EPA) Method 1 was used for selection of velocity traverse point locations.

EPA Method 2 was used for conducting stack gas pitot tube measurements used in determination of stack gas velocity.

EPA Method 3a was used for determination of oxygen (O_2) and carbon dioxide (CO_2) concentrations.

EPA Method 4 was used for determination of stack gas moisture content.

EPA Method 10 was used for determination of carbon monoxide (CO) concentrations.

SUMMARY OF RESULTS

GaPac owns and operates Georgia-Pacific Palatka Operations facility in Palatka, Putnam County, Florida. At this facility a wet scrubber is used to collect and control emissions from the Bleach Plant in the bleaching process of wood pulp. The emissions from this scrubber are the subject of this report.

Table 2 is a summary of the testing results for the emissions from the wet scrubber. The summary table contains data recorded during the test from the process feed rate and scrubber operation as supplied by GaPac personnel, ambient conditions, and the measured emissions. The emission rates for CO are reported in terms of parts per million by volume (ppmv) on a dry basis and pounds per hour (lbs/hr).

TABLE 2: Summary of Results
Bleach Plant Scrubber - Softwood Testing

Test Run No.	Run1	Run 2	Run 3	1
Date	10/28/02	10/28/02	10/28/02	
Start Time	09:34	11:27	13:17	
Stop Time	10:34	12:27	14:17	
Unit@peration 2		和ははは		Averages
Wood Type	Softwood	Softwood	Softwood	-
Production Rate (adtbph)	49.7	49.7	35.0	44.8
#ClO ₂ (adtbp)	45.8	46.8	49.9	47.5
Ambient Conditions	是不可能的	克里		
Atmospheric Pressure ("Hg)	29.98	29.96	29.91	29.95
Temperature (°F): Dry bulb	80.5	84.2	87.6	84.1
(°F): Wet bulb	75.5	74.3	74.8	74.8
Humidity (lbs moisture/lb air)	0.0174	0.0155	0.0151	0.0160
Measured Emissions	は、これによるである。 関するとは、 では、これは、 では、これには、 では、これには、 では、これには、 では、これには、 には、 には、 には、 には、 には、 には、 には、 には、 には、	に対して		
CO (ppmv, dry basis)	955.3	1083.6	951.3	996.7
O ₂ (% volume, dry basis)	20.76	20.67	20.69	20.71
CO ₂ (% volume, dry basis)	1.04	1.22	1.03	1.10
Stack Volumetric Flow Rates	建工		The state of the s	
via Pitot Tube (SCFH, dry basis)	7.70E+05	8.06E+05	8.19E+05	7.98E+05
Mass Emission Rates		State of the second		神子 まずる
CO (lbs/hr)	53.5	63.5	56.7	57.9

Please note that C102 Application Rate is considered Confidential Business Information

Three one-hour test runs were conducted for each required EPA test method on the wet scrubber outlet. CO, O₂, and CO₂ emissions were continuously monitored during each of these runs. Moisture content was determined gravimetrically during each test run using a chilled water impingement system. Stack velocity measurements were performed during each test run.

Pollutant mass emission rates were calculated using the volumetric flow rates determined by EPA Methods 1-4. Examples of mass emission rate calculations and other calculations necessary for the presentation of the results of this section are contained in Appendix B.

Appendix A contains all field data sheets used during these tests. Appendix B contains examples of all calculations necessary for the reduction of the data presented in this report. Operational data obtained during the testing is presented in Appendix C. Records of quality assurance activities are in Appendix D. Certifications of calibration gases and equipment used to conduct tests at this facility are in Appendix E. Appendix F contains a copy of the logged data records of the analyzer monitored emission concentrations.

PROCESS DESCRIPTION

Georgia-Pacific Corporation owns and operates the Georgia-Pacific Palatka Operations facility. In operation since 1947, this pulp and paper mill produces natural and bleached Kraft paper grades. The emissions from the outlet of the wet scrubber located at the Bleach Plant, a stage of the manufacture of bleached Kraft paper products, were measured as an engineering study to determine the effects of bleaching softwood pulp in lieu of hardwood pulp in the system. This section of the report provides a brief description of the process and the wet scrubber outlet.

The bleaching process is an elemental chlorine-free (ECF) process. The process utilizes ClO_2 for the pulp bleaching process. No elemental chlorine or hypochlorite salts are used in the process. The ClO_2 is produced on site.

The bleaching process consists of the staged introduction of ClO₂ to the pulp slurry followed by washing of the bleached pulp. G-P Palatka utilizes a 3-stage bleach plant for this process. The pulp comes across a pre-washer, followed by the D0 stage where ClO₂ is introduced, the E or extraction stage, and the D1 stage where additional ClO₂ is applied. The off gases from all stages of the process are collected and passed through a wet scrubber utilizing an alkaline scrubbing solution.

Sample ports meeting the criteria of EPA Method 1 were located in a straight vertical section of the scrubber stack outlet. The sample ports were greater than 2 stack diameters upstream from the nearest flow disturbance, the elbow just prior to the stack outlet, and greater than 8 diameters downstream from the nearest flow disturbance. Access to the stack was made available via a permanent steel frame platform equipped with a caged safety ladder. The diameter of the exhaust stack was 41.75 inches. Appendix A contains a field sketch of the stack configuration and sample port locations.

GaPac personnel provided operational data from the process instrumentation. Data sets were recorded during each test run; the average of this data was recorded in the summary table. Copies of the original data are contained in Appendix C of this report.

ANALYTICAL TECHNIQUE

The emissions from a bleach plant scrubber were measured to determine the quantity of emissions being emitted to the atmosphere under various operating conditions. The sampling and analysis procedures used during these tests conformed with those outlined in <u>The Code of Federal Regulations</u>, Title 40, Part 60, Appendix A, Methods 1, 2, 3a, 4, and 10. This section of the report describes the analytical techniques and procedures used during the testing.

The test matrix for the scrubber outlet consisted of three one-hour test runs following each test method specified by GaPac. The stack gas was analyzed for CO, O₂, and CO₂ by continuous instrumental monitors. All exhaust gas analyses were performed on a dry basis. Table 3 lists the instruments and detection principles used for these analyses.

Provisions were made to introduce the calibration gases to the instrumental monitors via two paths: 1) directly to the instruments via the sample manifold quickconnects and rotameters, and 2) through the complete sampling system including the sample probe, filter, heat trace, condenser, sample line, manifold, and rotameters. The former method was used for quick, convenient calibration checks. The latter method was used to demonstrate that the sample was not altered due to leakage, reactions, or adsorption within the sampling system (sample system bias check). An O, standard calibration gas was introduced into the O, analyzer directly. Then the response from the O₂ analyzer was noted as the calibration gas was introduced at Any difference between the two responses in the instrument was attributed to the bias of the sample system. Following the span gas bias check, a zero gas bias check was performed on the O, analyzer using nitrogen to check for any zero gas bias of the sample system. In accordance with EPA Method 3a, this span and zero bias check procedure was repeated for the CO₂ analyzer. procedure was also used for the CO analyzer although not required by EPA Method 10.

As shown in Figure 1, a 1-inch diameter stainless steel probe was inserted into the sample port of the stack. The gas sample was continuously pulled through the probe and transported via a 100-foot long. $\frac{7}{8}$ -inch diameter heat-traced Teflon® line into the mobile laboratory using a stainless steel/Teflon® diaphragm pump. At the pump exit the pressurized sample was pushed into a heated sample manifold. The bulk of the gas stream then passed into a stainless steel minimum contact condenser to dry the sample stream and into the (dry) sample manifold. From the manifold, the sample was partitioned to the analyzers through glass and stainless steel rotameters for flow control of the sample.

Instrumental monitors were housed in an air-conditioned trailer-mounted mobile laboratory. Gaseous calibration standards were provided in aluminum cylinders with concentrations certified by the vendor. EPA Protocol No. 1 was used to determine the cylinder concentrations where applicable (i.e., NO_X calibration gases).

EPA Method I was used to determine the velocity traverse point locations. Prior to conducting the tests, a cyclonic flow check was conducted. No significant cyclonic flow was encountered. The stack met the minimum criteria set forth in the method. Pitot tube measurements were made at eight (8) separate traverse points in each stack cross section for a total of sixteen (16) traverse points. The location of the sample ports and the pitot tube traverse point distances for the scrubber stack are denoted in the "Circular Stack Sampling Traverse Point Layout" data sheet, see Appendix A.

EPA Method 2 was used for determination of stack gas velocity during each run. A pitot tube and inclined gauge oil manometer were used to measure the differential pressure at each traverse point. The stack temperature was determined with a K-type thermocouple and digital thermometer.

The stack gas analyses for CO₂ and O₂ concentrations were performed in accordance with procedures set forth in EPA Method 3a. Instrumental analyses were used in lieu of an Orsat or Fyrite procedure due to the greater accuracy and precision provided by the instruments. The CO₂ analyzer was based on the principle of infrared absorption. The O₂ analyzer operated using a paramagnetic detector.

EPA Method 4 was used to measure the moisture content of the stack gas. A chilled water impingement system was used in conjunction with a calibrated dry gas meter to pull a sample greater than 21 scf coincident with each test run. A K-type (chromel-alumel) thermocouple was used in conjunction with a digital thermometer to determine the exit temperatures in the chilled water impingement sampling train. This parameter is measured to ensure that the gas stream is cooled to a minimum of 68 degrees Fahrenheit as required by sampling methodology. Determination of the moisture content was necessary to determine stack gas molecular weights and volumetric flow rates.

CO emission concentrations were quantified in accordance with procedures set forth in EPA Method 10. A continuous non-dispersive infrared (NDIR) analyzer was used for this purpose. This reference method analyzer was equipped with a gas correlation filter that removes most interference from moisture. CO₂, and other combustion products.

All data from the continuous monitoring instruments were logged into a computer file in 1-minute intervals and rolling 1-minute averages. A data logging system with a computer generated display screen monitored, recorded and averaged the emission concentrations. The program controlling the logging of data was also

used to log QA data. See Appendix F of this report for copies of the raw data and Appendix D for the QA data.

Cubix personnel collected ambient absolute pressure, temperature and humidity data. A wet/dry bulb sling psychrometer was used to determine ambient temperature and humidity conditions. An aircraft-type aneroid barometer (altimeter) was used to measure absolute atmospheric pressure.

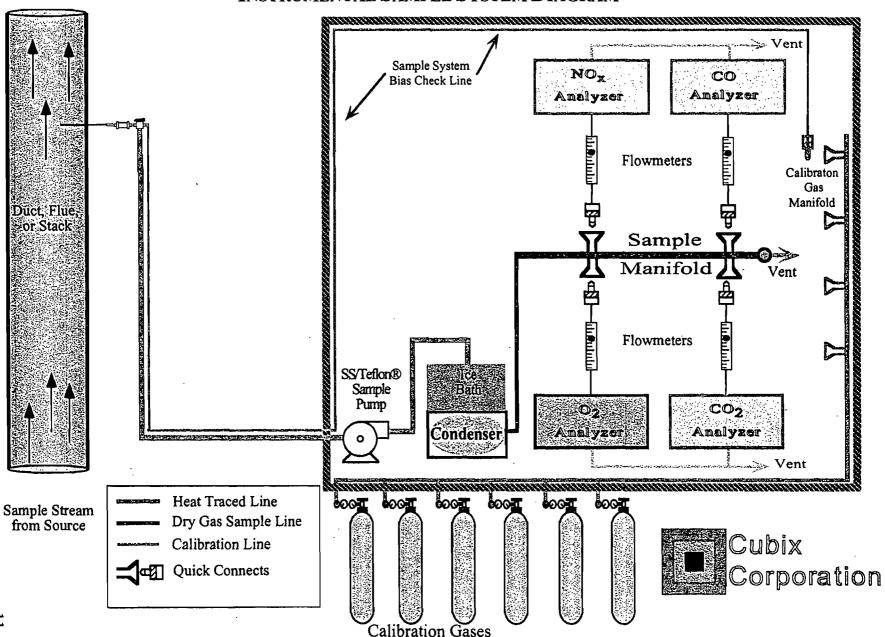
Emission calculations were conducted by a computer spreadsheet as shown in Table 2 of this report. Example calculations were performed manually using a hand-held calculator in order to verify the formulas used in the spreadsheet. Example calculations are in Appendix B of this report.

TABLE 3
ANALYTICAL INSTRUMENTATION

Parameter	Model and Manufacturer	Common Use Ranges	Sensitivity	Response <u>Time (sec.)</u>	Detection Principle
СО	TECO Model 48C	0-1 ppm 0-10 ppm 0-30 ppm 0-50, 0-100 ppm 0-200 ppm 0-500 ppm 0-1000 ppm	0.1 ppm	60	Infrared absorption, gas filter correlation detector, microprocessor based linearization.
CO ₂	Servomex 1400	0-5% 0-10% 0-15%	0.025% 0.05% 0.075%	< 10	Non-dispersive infrared absorption, electronic linearization of a logarithmic signal (Beer's Law)
O ₂	Servomex 1400	0-5% 0-10% 0-25%	0.02% 0.02% 0.02%	< 10	Paramagnetic cell detector, inherently linear.

NOTE: Higher ranges available by sample dilution.
Other ranges available via signal attenuation.

FIGURE 1
INSTRUMENTAL SAMPLE SYSTEM DIAGRAM



QUALITY ASSURANCE ACTIVITIES

A number of quality assurance activities were undertaken before, during and after this testing project. This section of the report in conjunction with the documentation in Appendix D describes each of those activities.

Each instrument's response was checked and adjusted in the field prior to the collection of data via a multi-point calibration. The instrument's linearity was checked by first adjusting the instrument's zero and span responses to zero nitrogen and an upscale calibration gas in the range of the expected concentrations. The instrument response was then challenged with other calibration gases of known concentration. For CO, O_2 , and CO_2 , the instrument's response was accepted as being linear if the response of the other calibration gases agreed within $\pm 2\%$ span of the predicted values. The responses of the infrared absorption type CO and CO_2 analyzers are made linear through electronic suppression.

System bias checks were performed both before and after the sampling system was used for emissions testing. The sampling system's integrity was tested by comparing the responses of the O₂ analyzer to a calibration gas (and a zero gas) introduced via two paths as previously described in the *Analytical Techniques* section of this report. This system bias test was performed to assure that no alteration of the sample had occurred during the test due to leakage, reactions, or absorption. Similarly, system bias checks were performed with CO and CO₂ for added assurance of sample system integrity. Examination of the logged QA data records and Instrumental Analysis Quality Assurance Data worksheet in Appendix D shows that the analyzer response via both sample paths agreed within ±5%.

The residence time of the sampling and measurement system was estimated using the pump flow rate and the sampling system volume. The pump's rated flow rate is 0.8 scfm at 5 psig. The sampling system volume was approximately 0.175 scf. Therefore, the minimum sample residence time was approximately 13 seconds.

Cubix Corporation and instrument vendors conducted interference response tests on the CO, O_2 , and CO_2 analyzers. The sum of the interference responses for H_2O , C_3H_8 , CO, CO_2 and O_2 is less than 2 percent of the applicable full-scale span value. The instruments used for the tests meet the performance specifications for EPA Methods 3a and 10. The results of the interference tests are available in Appendix D of this report.

The sampling system was leak checked by demonstrating that it could hold a vacuum greater than 15 inches of mercury (Hg) for at least 1 minute with a decline of less than 1 inch Hg. A leak test was conducted after the sample system was set

up and before testing began and after testing was completed before the system was dismantled. This test was conducted to insure that ambient air was not diluting the sampling system. The actual vacuum was greater than 24 inches Hg during the leak tests with no leakage detected.

As a minimum, before and after each test run, the analyzers were checked for zero and span drift. This allows test runs to be bracketed by calibrations and documents the precision of the data just collected. Calibration gases were introduced to the analyzers through the entire sampling system. Based on the applicable test method, the criterion for acceptable data is that each instrument drifts no more than $\pm 3\%$ of the full-scale response. Appendix D contains quality assurance tables and logged QA calibration records that summarize the zero and span checks that were performed for each test run. The worksheets also contain the data used to correct the data for drift per EPA Method 6c, Equation 6c-1. O₂ and CO₂ emissions data were corrected for drift as required by the test methods. CO emissions data was also corrected for drift to provide more accurate results and consistent quality assurance procedures.

The control gases used to calibrate the instruments were analyzed and certified by the compressed gas vendors to $\pm 1\%$ accuracy for each calibration gas. EPA Protocol No. 1 was used, where applicable (i.e., NO_x gases), to assign the concentration values traceable to the National Institute of Standards and Technology (NIST), Standard Reference Materials (SRM's). The gas calibration sheets as prepared by the vendor are contained in Appendix E.

The pitot tube tips used during the testing were visually inspected to insure that they met the criteria of EPA Method 2. The pitot tube lines were leak checked in the field in accordance with EPA Method 2 guidelines each time connection to the oil manometer was made.

The working dry gas meter used for the moisture train was calibrated prior to testing in accordance with EPA Method 4. A laboratory grade dry gas meter calibrated against a NIST reference instrument, a bell prover, was used for this calibration. Calibration certification documentation of the working meter can be found in Appendix E.

Appendix E also contains calibration data on ancillary measurement equipment used during this testing. The altimeter/barometer was used for determination of atmospheric pressure. Thermometers and thermocouples were used to determine stack gas temperatures and moisture train temperatures.

Cubix collected and reported the enclosed test data in accordance with the procedures and quality assurance activities described in this test report. Cubix makes no warranty as to the suitability of the test methods. Cubix assumes no liability relating to the interpretation and use of the test data by others.

APPENDIX A: FIELD DATA SHEETS

Sign In Sheet

Job Name: GEORGIA-	<u> PACIFIC - PALATKA PLA</u>	NT Date(s): OCTOBER 28, 2002
Job Number: Cusix	# 7382	Permit No. NA
Plant Name/Location:	GEORGIA-PACIFIC Corp. PA	CR 216 LATKA OPENATIONS /PALATKA, RUTNAM CO, F
Emission Source(s):	BLEACH PLANT WET	Scrusben
PARTICIPANTS:	Cubix Corporation	Test Contractor
	GEORGIA PACIFIC COSP.	Owner/Operator Regulatory Agency
		-

			Phone	Job Safety
Name	Affiliation	Position	Number	Review(Y/N)
Roger Paul Osier	C UZi X	Provict FOREMAN	(352)378-0332	У
Jim Hastings	Cuaix	FIELD TECH.	(352) 378-0332	у
JOE TAYLOR	GEORGIA PACIFIC	TEST COOLDINATOR	(386)329-0027	γ
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Cubix Corporation Air Emission Testing Job Safety Analysis

Date:	October 27th	and 28th, 2002	•		Description of To			
Mobile Lab/Cubix Crew:	T-13/LJB, RE	O, DLD, and JT	Н		Set-up on 10/27/02.	Tested wet sei	rubber outlet stack	at the Bleach
Client:	Georgia-Paci	fic Corporation		İ	Plant on 10/28 02.			
Job #/Contact:	7382-FL1/Joe	Taylor			, ,			
Plant Name:		fic Palatka Opera	itions					
Unit Name(s):	Bleach Pplan	•						
` '	Palatka, Flori							
Location (city/state): Permits Required	Talatka. 1 1011	Comments			Personal Protective	Fauinment F	Required	
Hot Work	Check	No permits requ	uired in area w	here we	hard hat	Check	acid suit	Check
Cold Work	Chack	were working.			ear plugs/mutis	Check	rubber boots	Check
Lock & Tag	Check	-			safety glasses	Check	monogoggles	Check
Scaffolding	Check				steel toed shoes	Check	face shield	Check
Crane/Lift	Check				gloves	Check	safety harness	Check
Line Break	Check				hot gloves	Check	respirator 🔮	Check
Emergency Response					Phone No's. & Aları			1)
Safe Haven:	Upw	ind	(Control room?	Plans office?	Plant Contact Ph.:			
Wind Direction:	Eas	it .	N NE E SE S	SW W NW	Control Room Ph.:		Fire:	
Evacuation Route:	Upw	-	from: gate? Back ga				All Clear:	
Assembly Points:	Down th	_	office? Down		Other:		Poison Gas: y	
Plant Map Reviewed:	Not App	-10-1	Yes or No or No		If facility has no alar		_	
Emergency Equipment I Emergency Shut Off	· —		،		There was a plant ala	rm for chlorin	ne gas but they did	t know what the
Fire Extinguisher	Located	Not Applicable	manual emerg Cubix Mobile Lab		alarm sounded like	They said we	would know if we	heard it
Safety Showers	Located Located	Not Applicable	required for		alami sounded like	They said we	"Ould know if "C	neard it.
Escape Air Pack	Located	Not Applicable	required for	-				
		DIDENTIFIE			PRECAUT	CIONS TO	BE IMPLEME	NTED
Hazardous Material (in	plant area)	List Hazmat??	C1O2.		Cubix MSDS in Mob	ile Lab	Yes No	
(flammability, reactivity, health	hazards)	1			Plant MSDS reviewe	d???	Yes Not	Available
Environmental Hazards					Protective Equ	ipment	Protective	e Actions
airbome particulate	Present	No Hazard	Comments: D	ifficult	respirator	Check	OTHER	Check
burn hazard	Present	No Hazard	access to stack	c and	work gloves	Check	shade/cool breaks	Check
rain / fog	Present	No Hazard	sample ports.		rain protect elect, equip.	Check	rain gear	Check
electrical shock	Present	No Hazard			inspect extension cords	Check	secure/protect ext.co	rds Check
heat stress	Present	No Hazard			hot gloves	Check	warm up breaks	Check
cold weather/frostbite	Present	No Hazard			cold weather clothing	- C C C.	liquid intake	Check
inadequate lighting	Present	No Hazard			flash light/head lamp	THE PART OF STREET	night lighting	Check
noise	Present	No Hazard			hearing protection	Check	hard hat liner alternate route	Check
poor access/egress	Presenta	No Hazard		<u></u>	housekeeping	Check		Checks
	ards (check h	azards that are pr			Respiratory Saf	h 40.5 \$7.50	Protective	Clothing
asfixiation	Check	carcinogen		Check	supplied fresh air	Check.	fire suit	Check
poison gas	Checks	chemical burns	Terror.	Check	SCBA	Check	acid suit	Check
chemical eye exposure	Checks	chemical skin e		Check3	respirator (correct type?)		rubber boots	Check
flammable gas	Check Check	flamable liquid	<u>_</u>	Checks Checks	escape pack exposure dosiometer	Check	monogoggles face shield	Check
strong acid	Check	strong base		Checki	OTHER	Check	OTHER	Check
					h			
		ing & Fall Haza					Protective Actions	
test equipment hoisting (p	uney/boom)	Required	= Not Applica		equipment secure	Check	clear lift zone	Check
portable ladder		= Required	Not Applica		operator certification		rope inspection body harness	Check
man lift (cherry picker)		= Required	Not Applica		guy lines	Check	•	= Check
personnel basket (crane) Plant Stairs & Ladders		= Required	= Not Applica		radios/handsignals	Check	guard rails, toe pl	_
	ilicle	Required	Not Applica		housekeeping Hines secure	- Check	monorails secure	Check
rigging sample lines, umb	mele	Required	_ Not Applica		rimes secure	Check Check	monorans secure	
scaffold		Required	Not Applica	ibie	secure tools	Check	hard hats	Check

Best Available Copy

Circular Stack Sampling Traverse Point Layout (EPA Method 1, Velocity Measurement Traverse Points)

Date: October 27th, 2002

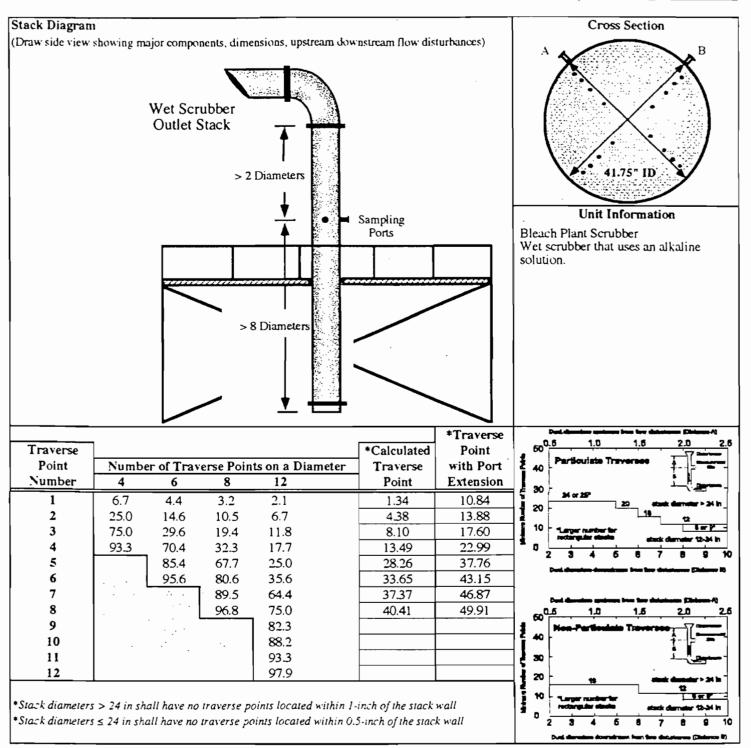
Client: Georgia-Pacific Corporation

Plant: G-P Palatka Operations

Source: Bleach Plant Scrubber

Technician(s): RPO, JTH

Port + Stack ID (in): 51.25
Port Extension (in): 9.50
Stack ID (in): 41.75
Stack ID (in): 41.75
Duct Diameters upstream from flow disturbance (A): > 2
Duct Diameters downstream from flow disturbance (B): >8
Total Required Traverse Points: 1.6
No. of Traverse Points per Diameter: 8



EPA Methods 1 through 4: Velocity, Moisture Content. Molecular Weight, and Volumetric Flow Rates

Test Run No.	Run 1	Run 2	Run 3
Date	10/28/02	10/28/02	10/28/02
Start Time (Moisture Run Times)	09:42	11:33	13:24
Stop Time (Moisture Run Times)	10:27	12:14	14:05
Stack Moisture & Molecular Wt. via EPA Methods 3a &	: 4		
O ₂ (% volume, dry basis)	20.76	20.67	20.69
CO ₂ (% volume, dry basis)	1.04	1.22	1.03
Beginning Meter Reading (ft')	675.970	703.905	739.319
Ending Meter Reading (ft')	703.495	726.224	762.465
Beginning Impingers Weight (g)	2235.2	2262.1	2285.0
Ending Impingers Weight (g)	2262.1	2285.0	2316.9
Dry Gas Meter Factor (K₀)	0.9869	0.9869	0.9869
Dry Gas Meter Temperature (°F begin)	96	84	88
Dry Gas Meter Temperature (°F end)	90.6	90	95
Atmospheric Pressure ("Hg, absolute)	29.98	29.96	29.91
Volume of Water Vapor Collected (SCF)	1.268	1.080	1.504
Volume of Air Metered (SCF)	25.964	21.281	21.851
Stack Gas Moisture (% volume)	4.66	4.83	4.50
Dry Gas Fraction	0.9534	0.9517	0.9550
Stack Gas Molecular Wt. (lbs/lb-mole)	28.48	28.49	28.50
Stack Flow Rate via Pitot Tube			
ΔP #1	0.13	0.14	0.18
ΔP #2	0.18	0.19	0.19
ΔP #3	0.22	0.23	0.22
ΔP #4	0.20	0.25	0.22
ΔP #5	0.24	0.27	0.23
ΔP #6	0.24	0.24	0.23
ΔP #7	0.18	0.24	0.25
ΔP #8	0.18	0.22	0.25
ΔΡ #9	0.18	0.17	0.19
ΔP #10	0.20	0.19	0.22
ΔP #11	0.21	0.23	0.23
ΔP #12	0.22	0.22	0.25
ΔP #13	0.19	0.19	0.21
ΔP #14	0.20	0.23	0.22
ΔP #15	0.18	0.22	0.21
ΔΡ #16	0.16	0.22	0.23
Pitot Tube Factor	0.84	0.84	0.84
Sum of Square Root of ΔP's	7.0355	7.4085	7.5071
Number of Traverse Points	16	16	16
Average Square Root of ΔP 's	0.439721	0.463030	0.469191
Average Temperature (°F)	126.8	130.9	130.8
Static Pressure ("H ₂ O)	-0.28	-0.14	-0.18
Stack Diameter (inches)	41.75	41.75	41.75
Stack Area (ft²)	9.507	9.507	9.507
Stack Velocity (ft/min)	1571	. 1660	1683
Stack Flow, wet (ACFM)	14936	15783	16005
Average Stack Flow, dry (SCFH)	7.70E+05	8.06E+05	8.19E+05

MOISTURE & VELOCITY FIELD DATA SHEET

Date: 15-7 X - CZ	Dry Gas Meter ID: 7-10 EquIMETER
Plant: G-P Pubtko Plant	Dry Gas Meter Factor: 0.9869 (Kd)
Source: Chlorne Plant Scrubber	Pitot Tube No/Type: #2110 .7' 33" W SS STYP
rechnicians: KPO JUTH	Pitot Tube Factor: 0.84
Atm. Pressure: 29.78 "Hg (Ph)	Static Pressure: 28 "H ₂ O (Pg)
Test Run No.: Run 1	Ave. Stack Temp. 126.8 'F (Ts)

Collection Data

Sample Box	' /				
Leak Check	$\leq 0.02 \text{ ft}^3$	/min			
Pre-Test	0.000	ft ³ /min			
Leak Check	24. A	'Hg Vac.			
Post-Test	Ø 000	ft ³ /min			
Leak Check	25.0	'Hg Vac.			
	Initial	Final			
Time	9:42	10.27			
DGM Reading	675.970	703.495			
(ft ³ or L)					
DGM Average	96	90.6			
Temp (°F)	10	70.0			
Last Impinger	66	624			
Temp. (°F)	66				
DGM Flow Rate	- 40	48			
O ₂ (% vol.)					
CO ₂ (% vol.)					

Velocity System Leak Check

Leak Check ≤ 0.1 "H ₂ O/min				
at a pressu	re ≥ 3.0 "H ₂ O			
Pre-Test	0.0 0.0 "H ₂ O/min			
Leak Check	3.6 4.6 H ₂ O Pres.			
Post-Test	0.0 0.0 H2O/min			
Leak Check	4.2 4.1 "H2O Pres.			

Impingment System

Impinger	Contents	Initial Weight	Final Weight
1	10:420	545.7	565.0
2	DIHO	557.5	559.8
3 -	Émply.	485.9	486.5
4	Sicell	646.1	650.8
5			•
6			
Totals		2235.2	2262,1

Velocity Traverse Data with Stack Temperature and Cyclonic Flow Check

with Stack Temperature and Cyclonic Flow Check							
Point	ΔP ("H ₂ O)	°F	α	Point	ΔP ("H ₂ O)	cF	C/.
1-1	,/3	125	5	2-1	18	122	/ O
1-2	.18_	125	10	2-2	, 2ర	123	
1-3	ノ マス	125	10	Z-3	.21	127	7
1-4	,20	126	5	2.4	. ス೩	128	5 ,
1.5	,24	126	6	25	./9	130	6
1-6	. 24	126	8	2.6	. 20	130	
17	. 18	126	8	2-7	.18	132	5
1-8	./8	126	10	15.8	.16	132	10
		ļ					
		ļ	ļ	<u> </u>			
			<u> </u>	<u>;</u>			
	-	ĺ		,			
			<u> </u>				
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MOISTURE & VELOCITY FIELD DATA SHEET

Date: 10-28-2002

Plant: 6-P PALATKA PLANT

Source: Chlorine Plant Scrubber

Technicians: RPO, UTH

Atm. Pressure: 29.96 "Hg (Pb)

Test Run No.: RUN 2

Dry Gas Meter ID: 7-10 EQUIMETED

Dry Gas Meter Factor: 0,9869 (Kd)

Pitot Tube No/Type: \$\frac{210}{7\sqrt{3}\sqrt{0}\sqrt{3}\sqrt{0}\sqrt{3}\sqrt{0}\sqrt{3}\sqrt{0}\sqrt{2}\sqrt{0}\sqrt{3}\sqrt{0}\sqrt{2}\sqrt{0}\sqrt{3}\sqrt{0}\sqrt{2}\sqrt{0}\sqrt{2}\sqrt{0}\sqrt{2}\sqrt{0}\sqrt{2}\sqrt{0}\sqrt{2}\sqrt{0}\sqrt{2}\sqrt{0}\sqrt{2}\sqrt{0}\sqrt{2}\sqrt{0}\sqrt{2}\sqrt{0}\sqrt{2}\sqrt{0}\sqrt{2}\sqrt{0}

Collection Data

Sample Box	1	
Leak Check	$\leq 0.02 \text{ ft}^3$	/min
Pre-Test	0.000	ft ³ /min
Leak Check	22.5	"Hg Vac.
Post-Test	0.000	ft ³ /min
Leak Check	ه .2 3	"Hg Vac.
	Initial	Final
Time	1133	12:14
DGM Reading	703,905	726.224
(ft ³ or L)		
DGM Average	34	90
Temp (°F)		/ 0
Last Impinger	67	58
Temp. (°F)		00
DGM Flow Rate	40	40
O ₂ (% vol.)		
CO ₂ (% vol.)		

Velocity System Leak Check

Leak Check	≤ 0.1 "H ₂ O/min
at a pressu	re ≥ 3.0 "H ₂ O
Pre-Test	0.0 0.0 "H ₂ O/min
Leak Check	36 46"H2O Pres.
Post-Test	0.0 0.0 "H ₂ O/min
Leak Check	4.2 4.1 "H2O Pres.

Impingment System

Impinger	Contents	Initial Weight	Final Weight
1	D1 /20	566.0	582.6
2	AHZO	559.8	561.7
3	MT	486.5	486.8
4	S, GEL	650,8	653.9
5			
6			
Totals		3262.	2285.0

Velocity Traverse Data with Stack Temperature and Cyclonic Flow Check

		cmpe	atu		yelollie x lo		
$Point \Delta P$	("H ₂ O)	°F	CX.	Point	ΔP ("H ₂ O)	°F	α
1-1 .	14	129		2-1	,17	133	
1-2 1	9	129		2-2	.19	133	
1-3	23	131		2-3	, 23	133	
1 1		132		2-4	, 22	133	
1-5	27	133		2-5	-19	/3/	
1-6.	24	134		2.6	,23	130	
1-7	24	134		2-7	.22	125	
1-8	22	133	V	a-8	,22	12!	ψ_{\perp}
							_
	-						

MOISTURE & VELOCITY FIELD DATA SHEET

Date: 10-28-2002

Plant: CP PALATKA PLANT

Source: Chloring Plant Scrusber

Technicians: RPO, JTH

Atm. Pressure: 29.91 "Hg (Pb)

Test Run No.: RUN 3

Dry Gas Meter ID: T-10 EQUIMETER.

Dry Gas Meter Factor: 0,9869 (Kd)

Pitot Tube No/Type: #2110 71/238100 55 51786

Pitot Tube Factor: 0,84

Static Pressure: 1-18 "H₂O (Pg)

Ave. Stack Temp. /30,8 °F (Ts)

Collection Data

$\leq 0.02 \text{ft}^3$	/min
0.000	ft ³ /min
25.0	'Hg Vac.
0.000	ft ³ /min
25.5	"Hg Vac.
Initial	Final
13:24	14:05
739.319	762.
	465
188	95
	75
16	1.11
66	64
40	40
	0.000 25.0 0.000 25.5 Initial /3:24 739.319

Velocity System Leak Check

		Edit Check
Leak Check	≤ 0.	1 "H ₂ O/min
at a pressu	re ≥	3.0 "H ₂ O
	┷	
Pre-Test	p.0	o∙o "H2O/min
Leak Check	36	4.6 "H2O Pres.
	+	
Post-Test	0.0	0.0 H2O/min
	ا م ا	41 1 1177 0 5
Leak Check	9.2	4.1 "H2O Pres.

Impingment System

Impinger	Contents	Initial Weight	Final Weight
1	DiHzo	*84.6	605.0
2	D; H20	561.7	565.6
3	MT	486.8	487.7
4	SiGEL	653.9	658.6
5			
6			
Totals		2285	2316.9

Velocity Traverse Data with Stack Temperature and Cyclonic Flow Check

						y clottic x to		
Point	ΔP ("H ₂ O)	°F	Cr.		Point	$\Delta P ("H2O)$	°F	C.
1-1	.18	129			2-1	.19	130	
1-2	.19	129			2-2	.22	130	
1-3	,22	2/3/		ļ	2-3	. 23	131	
1-4	.22	131			24	, 25	132	
1-5	, 23	131		j	2-5	, 21	131	
1-6	23	132			2.6	, 22	131	
1-7	. 25	131			2.7	. 2/	/3/	
1-8	£3.25	13	\vee	į	2-8	,23	13/	V
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				1				
		-	-				-	$\overline{}$

APPENDIX B: EXAMPLE CALCULATIONS

EXAMPLE CALCULATIONS

Moisture Content via EPA Method 4

refers to Test Run # 1

```
= net impinger weight gain = 2262.1 \text{ g} - 2235.2 \text{ g}
                                                                             = 26.9 g
M_{WC}
Y
            = dry gas meter correction factor
                                                                             = 0.9869
                                                                             = 27.525 \text{ ft}^3
V_{\rm m}
            = volume metered = (703.495 - 675.970)
            = atmospheric pressure
                                                                             = 29.98 \text{ "Hg}
Patm
            = average meter pressure = Patm
                                                                             = 29.98 \text{ "Hg}
Pmer
            = average meter temperature = 93.3° F + 460 °F
                                                                             = 553.3^{\circ} R
T_{met}
            = conversion factor, water weight to vapor
K_2
                                                                             = 0.04715 \text{ ft}^{-3}/\text{g}
            = standard temp, pressure (STP) correction factor
                                                                            = 17.64^{\circ} \text{ R/ "Hg}
Kз
```

$$V_{WC}$$
 = total volume of water vapor collected at STP

 $= K_2 \times M_{WC}$

 $= (0.04715 \times 26.9)$

 $= 1.2683 \text{ ft}^3$

$$V_{m(std)}$$
 = total volume metered at STP

$$= K_3 \times Y \times V_m \times \frac{P_{met}}{T_{met}}$$

=
$$17.64 \times 0.9869 \times 27.525 \times \frac{29.98}{553.3}$$

$$= 25.964 \text{ ft}^3$$

$$B_{ws}$$
 = moisture content by EPA Method 4

$$= \frac{V_{WC}}{V_{WC} + V_{STP}}$$

$$= \frac{1.2683}{1.2683 + 25.964}$$

$$B_{WS} = 0.04657$$

= 4.66 % moisture

Stack Gas Molecular Weight

Refers to Test Run # 1

```
= 18 lb/lb-mole
MW_{H,O}
            = molecular wt of H<sub>2</sub>O
MW_{CO}
            = molecular wt of CO<sub>2</sub>
                                                         = 44 \text{ lb/lb-mole}
MW_{O}
            = molecular wt of O_2
                                                         = 32 lb/lb-mole
MW_N
                                                         = 28 lb/lb-mole
            = molecular wt of N_2
C_{CO}
            = concentration of CO<sub>2</sub>
                                                         = 0.0104 (from analyzer)
C_{O}
            = concentration of O_2
                                                         = 0.2076 (from analyzer)
            = concentration of N_2
                                                         = 1 - (C_{CO_2} + C_{O_2}) = 0.782
C_{N}
                                                         = 0.95343
F_d
            = dry gas fraction = 1 - B_{ws}
                = molecular weight of stack gas (lb/lb-mole)
                 = wt. of H_2O + wt. of CO_2 + wt. of O_2 + wt. of N_2
                = (MW_{H_2O} \times B_{ws}) + (F_d \times ((MW_{CO_2} \times C_{CO_2}) + (MW_{O_2} \times C_{O_2}))
                          + (MW_{N_1}, x C_{N_2})))
                 = (18 \times 0.04657) + (0.95343 \times ((44 \times 0.0104) + (32 \times 0.2076))
                         + (28 \times 0.782))
        MW
               = 28.48(4) \text{ lb/lb-mole}
```

Stack Gas Flow Rate via Pitot Tube, Qd

Refers to Test Run # 1

$$\begin{array}{lll} C_{p} & = & \text{pitot tube coefficient} & = & 0.84 \\ \Delta P & = & \text{pressure difference in stack as measured (in. H_{2}O)} \\ \sqrt{\Delta P_{av}} & = & \text{average of square root of } \Delta P's & = & 0.439721 \\ T_{S} & = & \text{ave. stack temperature} & = & 126.8^{\circ} \, \text{F} + 460 & = & 586.8^{\circ} \, \text{R} \\ P_{atm} & = & \text{site corrected atmospheric pressure} & = & 29.98 \text{ "Hg} \\ P_{g} & = & \text{stack static pressure} & = & 29.98 \text{ "Hg} \\ P_{g} & = & \text{stack static pressure} & = & 29.959 \text{ "Hg} \\ P_{g} & = & \text{absolute stack pressure} & = & 29.959 \text{ "Hg} \\ P_{g} & = & \text{pitot tube constant} & = & 85.49 \, \frac{\text{ft}}{\text{sec}} \left(\frac{(\text{lb/lb} - \text{mole})(\text{in.Hg})}{({}^{\circ}\text{R})(\text{in.H}_{2}O)} \right)^{\frac{1}{2}} \\ P_{std} & = & \text{absolute Temperature} & = & 528^{\circ} \, \text{R} \\ P_{std} & = & \text{standard atmospheric pressure} & = & 29.92 \, \text{"Hg} \\ V_{s} & = & \text{stack velocity (ft/sec)} \\ & = & K_{p} \, \text{x} \, C_{p} \, \text{x} \, \sqrt{\Delta P_{av}} \, \text{x} \, \sqrt{\frac{T_{s}}{(P_{s} \, \text{x} \, \text{MW})}} \\ & = & 85.49 \, \text{x} \, 0.84 \, \text{x} \, 0.439721 \, \text{x} \, \sqrt{\frac{586.8}{(29.959 \, \text{x} \, 28.484)}} \\ & = & 26.185 \, \text{ft/sec} \, \text{x} \, 60 \, \text{sec/min} \\ V_{s} & = & 1571.1 \, \text{ft/min} \\ Q_{a} & = & \text{stack flow rate (ft}^{3}/\text{min, actual})} \\ & = & V \, \text{x} \, \text{A} \, \text{, where A} = \text{area of stack} = & 9.507 \, \text{ft}^{2} \\ Q_{a} & = & 1571.1 \, \text{x} \, 9.507 = 14936.4 \, \text{ft}^{3}/\text{min} \\ Q_{d} & = & \text{average stack flow rate on a dry basis at standard conditions (DSCFH)} \\ & = & \frac{Q_{a} \, \text{x} \, T_{3d} \, \text{x} \, P_{a}}{T_{s} \, \text{x}} \, \text{x} \, F_{d} \, \text{x} \, 60 \\ & = & \frac{14936.4 \, \text{x} \, 528 \, \text{x} \, 29.959}{586.8 \, \text{x} \, 29.92} \, \text{x} \, 0.95343 \, \text{x} \, \, 60 \\ & = & \frac{14936.4 \, \text{x} \, 528 \, \text{x} \, 29.959}{586.8 \, \text{x} \, 29.92} \, \text{x} \, 0.95343 \, \text{x} \, \, 60 \\ & = & \frac{14936.4 \, \text{x} \, 528 \, \text{x} \, 29.959}{586.8 \, \text{x} \, 29.92} \, \text{x} \, 0.95343 \, \text{x} \, \, 60 \\ & = & \frac{14936.4 \, \text{x} \, 528 \, \text{x} \, 29.959}{586.8 \, \text{x} \, 29.92} \, \text{x} \, 0.95343 \, \text{x} \, \, \, 60 \\ & = & \frac{14936.4 \, \text{x} \, 528 \, \text{x} \, 29.959}{586.8 \, \text{x} \, 29.959} \, \text{x} \, 0.95343 \, \text{x} \, \, \, 60 \\ & = & \frac{14936.4 \,$$

Correction of O₂ Gas Concentrations, CO₂

Refers to Test Run # 1

Analytical instruments tend to drift in their calibrations over time and with changes in atmospheric conditions. Span and zero gas bias drift checks (calibrations) were conducted prior to and following each test. The results of these calibrations were used to bracket and thus correct the raw gas concentrations into corrected (more accurate) gas concentrations. The calculation used for these correction is 40 <u>CFR</u> 60, Appendix A, Method 6c, Equation 6c-1. This correction is required for CO₂ exhaust concentrations when using Method 3a. Cubix also conducts this correction for EPA Method 10 in order to present more accurate and consistent test results.

 U_{O_1} = analyzer O_2 gas concentration, uncorrected for drift and bias

 U_{O_1} = 20.52 ppmv, uncorrected

C₀ = Average of initial/final zero gas concentrations

= -0.04 ppmv

C_m = Average of initial/final span gas concentrations

= 11.785 ppm v

C_{ma} = Actual upscale cylinder span gas concentrations

= 11.94 ppm v

 C_{O_2} = Effluent O_2 gas concentration, ppmv corrected

=
$$(U_{O_2} - C_0) \times \frac{C_{ma}}{C_m - C_0}$$

=
$$(20.52 + 0.04) \times \frac{11.94}{11.785 + 0.04}$$

 C_{O_2} = 20.76 ppmv O_2 , dry basis corrected

CO Mass Emission Rate (lbs/hr)

Refers to Test Run # 1

 C_{CO} = observed concentration of CO = 955.3 ppmv

 MW_{CO} = 28.01 lb/lb-mole for carbon monoxide

for ideal gas, 385.15 SCF = 1.0 lb/mole

 Q_d = 7.698 x 10⁵ SCFH (from ave. pitot tube volumetric flow)

 E_{CO} = mass emission rate of CO in (lb/hr)

=
$$C_{CO} \times 10^{-6} \times Q_d \times \frac{MW_{CO}}{385.15}$$

=
$$955.3 \times 10^{-6} \times 7.698 \times 10^{5} \times \frac{28.01}{385.15}$$

 $E_{CO} = 53.5 \text{ lbs/hr}$

APPENDIX C: OPERATIONAL DATA

PRODUCTION RATE DATA

RUN	DATE	TIME	SPECIES	PRODUCTION RATE,	#ClO2/adtbp
				adtbph	
1	10/28/02	0934-1034	softwood	497	45.8
2	10/28/02	1127-1227	softwood	49.7	46.8
3	10/28/02	1317-1417	softwood	35.0	49.9

Please note that the Chemical Application Rate is considered Confidential Business Information

APPENDIX D: QUALITY ASSURANCE ACTIVITIES

Quality Assurance Activities Calibration Error, Bias, and Drift Checks

Analyzer Range (ppmv), O, & CO, in % vol 1250.0 25.00 15.00 Strip Chart Offset 0.0 10.0 2.0 Low Level Certified Value (ppm or % vol) 253.0 4.53 4.48 Mid Level Certified Value (ppm or % vol) 441.0 11.94 7.99 High Level Certified Value (ppm or % vol) 885.0 20.90 12.62 Zero Target (% Chart) 0.0 10.0 2.0 Low Level Target (% Chart) 20.2 28.1 31.9 Mid Level Target (% Chart) 35.3 57.8 55.3 High Level Target (% Chart) 70.8 93.6 86.1	
Strip Chart Offset 0.0 10.0 2.0 Low Level Certified Value (ppm or % vol) 253.0 4.53 4.48 Mid Level Certified Value (ppm or % vol) 441.0 11.94 7.99 High Level Certified Value (ppm or % vol) 885.0 20.90 12.62 Zero Target (% Chart) 0.0 10.0 2.0 Low Level Target (% Chart) 20.2 28.1 31.9 Mid Level Target (% Chart) 35.3 57.8 55.3 High Level Target (% Chart) 70.8 93.6 86.1	
Low Level Certified Value (ppm or % vol) 253.0 4.53 4.48 Mid Level Certified Value (ppm or % vol) 441.0 11.94 7.99 High Level Certified Value (ppm or % vol) 885.0 20.90 12.62 Zero Target (% Chart) 0.0 10.0 2.0 Low Level Target (% Chart) 20.2 28.1 31.9 Mid Level Target (% Chart) 35.3 57.8 55.3 High Level Target (% Chart) 70.8 93.6 86.1	
Mid Level Certified Value (ppm or % vol) 441.0 11.94 7.99 High Level Certified Value (ppm or % vol) 885.0 20.90 12.62 Zero Target (% Chart) 0.0 10.0 2.0 Low Level Target (% Chart) 20.2 28.1 31.9 Mid Level Target (% Chart) 35.3 57.8 55.3 High Level Target (% Chart) 70.8 93.6 86.1	
High Level Certified Value (ppm or % vol) 885.0 20.90 12.62 Zero Target (% Chart) 0.0 10.0 2.0 Low Level Target (% Chart) 20.2 28.1 31.9 Mid Level Target (% Chart) 35.3 57.8 55.3 High Level Target (% Chart) 70.8 93.6 86.1	
Zero Target (% Chart) 0.0 10.0 2.0 Low Level Target (% Chart) 20.2 28.1 31.9 Mid Level Target (% Chart) 35.3 57.8 55.3 High Level Target (% Chart) 70.8 93.6 86.1	
Low Level Target (% Chart) 20.2 28.1 31.9 Mid Level Target (% Chart) 35.3 57.8 55.3 High Level Target (% Chart) 70.8 93.6 86.1	
Mid Level Target (% Chart) 35.3 57.8 55.3 High Level Target (% Chart) 70.8 93.6 86.1	
High Level Target (% Chart) 70.8 93.6 86.1	
Zero Observed (% Chart) 0.0 10.0 2.0	
Mid Level Observed (% Chart) 34.5 57.8 55.5	
High Level Observed (% Chart) 71.2 93.6 86.1	
Zero Observed (ppm or % vol) 0.33 0.00 0.00	
Low Level Observed (ppm or % vol) 244.64 4.50 4.52	
Mid Level Observed (ppm or % vol) 430.65 11.95 8.02	
High Level Observed (ppm or % vol) 889.46 20.90 12.62	
% Difference From Zero to Target 0.0 0.0	
% Difference From Low to Target 0.7 0.1 -0.3	
% Difference From Mid to Target 0.8 0.0 -0.2	
% Difference From High to Target -0.4 0.0	
EPA Allowable % Difference from Target ±2% Span ±2% Span ±2% Span	ın
Test Run 1 CO O ₂ CO	2
Analyzer Range (ppm), O ₂ & CO ₂ in % 1250.0 25.00 15.00	
Calibration Gas Certified Value (ppm or %) 885 11.94 7.99	
Strip Chart Offset 0.0 10.0 2.0	
Target Calibration Gas (Chart %) 70.8 57.8 55.3	
Actual Zero Gas from Direct (Chart %) 0.0 10.0 2.0	
Actual Calibration Gas from Direct (Chart %) 71.2 57.8 55.5	
Initial Readings	-
Zero Gas (chart %) -0.2 9.9 2.4	\dashv
Calibration Gas (chart %) 71.0 57.1 54.9	
Zero Gas (ppmv) -2.97 -0.03 0.06	
Calibration Gas (ppmv) 887.15 11.77 7.94	
Final Readings Zero Gas (chart %) -0.2 9.8 2.3	
Zero Gas (ppmv) -2.97 -0.05 0.04	1
Calibration Gas (ppmv) 888.80 11.80 7.98	
Bias and Drift Calculations	\longrightarrow
Zero Bias (% Chart) (Run-Direct Cal) ≤5% -0.3 -0.2 0.3	
Calibration Bias (% Chart) ≤5% -0.1 -0.6 -0.3	
Zero Drift (Chart %) (Run-Run) $\leq 3\%$ 0.0 0.1 0.1	
Zero Drift (Chart %) (Run-Run) $\leq 3\%$ 0.0 0.1 0.1 Calibration Drift (Chart %) $\leq 3\%$ -0.1 -0.1 -0.3	
Zero Drift (Chart %) (Run-Run) $\leq 3\%$ 0.0 0.1 0.1 Calibration Drift (Chart %) $\leq 3\%$ -0.1 -0.3 Run Results	
Zero Drift (Chart %) (Run-Run) ≤3% 0.0 0.1 0.1 Calibration Drift (Chart %) ≤3% -0.1 -0.1 -0.3 Run Results 76.7 92.1 9.2	
Zero Drift (Chart %) (Run-Run) $\leq 3\%$ 0.0 0.1 0.1 Calibration Drift (Chart %) $\leq 3\%$ -0.1 -0.3 Run Results	

Quality Assurance Activities Calibration Error, Bias, and Drift Checks

Test Run 2	CO	O_2	CO_2
Analyzer Range (ppm), O, & CO, in %	1250.0	25.00	15.00
Calibration Gas Certified Value (ppm or %)	885	20.90	4.48
Strip Chart Offset	0.0	10.0	2.0
Target Calibration Gas (Chart %)	70.8	93.6	31.9
Actual Zero Gas from Direct (Chart %)	0.0	10.0	2.0
Actual Calibration Gas from Direct (Chart %)	71.2	93.6	32.1
Initial Readings	· · · · <u>-</u>	-	
Zero Gas (chart %)	-0.2	9.8	2.3
Calibration Gas (chart %)	71.1	92.8	32.0
Zero Gas (ppmv)	-2.97	-0.05	0.04
Calibration Gas (ppmv)	888.80	20.70	4.50
Final Readings	000.00		4.50
Zero Gas (chart %)	-0.1	9.9	2.4
Calibration Gas (chart %)	71.4	92.5	31.9
Zero Gas (ppmv)	-1.40	-0.03	0.06
Calibration Gas (ppmv)	893.00	20.62	4.48
Bias and Drift Calculations	693.00	20.02	7.70
Zero Bias (% Chart) (Run-Direct Cal) ≤5%	-0.1	-0.1	0.4
Calibration Bias (% Chart) ≤5%	0.3	-0.1 -1.1	-0.3
Zero Drift (Chart %) (Run-Run) $\leq 3\%$	-0.1	0.1	-0.3
Calibration Drift (Chart %) (Kun-Kun) \$3%	-0.1 -0.3	0.3	0.1
Run Results	-0.3	0.3	0.1
Raw Results (chart %)	87.3	91.7	10.4
	1091.3	20.43	
Raw Results (ppmv or % vol)		20.43	1.26 1.22
Corrected Results (ppmv or % vol) from % chart	1083.6		1.22
I		\sim	\sim
Test Run 3	CO	O_2	CO_2
Test Run 3	1250.0	O ₂	CO ₂
	1250.0 885		
Analyzer Range (ppm), O ₂ & CO ₂ in %		25.00	15.00
Analyzer Range (ppm), O ₂ & CO ₂ in % Calibration Gas Certified Value (ppm or %)	885	25.00 20.90	15.00 4.48
Analyzer Range (ppm), O ₂ & CO ₂ in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset	885 0.0	25.00 20.90 10.0	15.00 4.48 2.0
Analyzer Range (ppm), O ₂ & CO ₂ in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %)	885 0.0 70.8	25.00 20.90 10.0 93.6	15.00 4.48 2.0 31.9
Analyzer Range (ppm), O ₂ & CO ₂ in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %)	885 0.0 70.8 0.0	25.00 20.90 10.0 93.6 10.0	15.00 4.48 2.0 31.9 2.0
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %)	885 0.0 70.8 0.0	25.00 20.90 10.0 93.6 10.0	15.00 4.48 2.0 31.9 2.0
Analyzer Range (ppm), O ₂ & CO ₂ in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings	885 0.0 70.8 0.0 71.2	25.00 20.90 10.0 93.6 10.0 93.6	15.00 4.48 2.0 31.9 2.0 32.1
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %)	885 0.0 70.8 0.0 71.2	25.00 20.90 10.0 93.6 10.0 93.6	15.00 4.48 2.0 31.9 2.0 32.1
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv)	885 0.0 70.8 0.0 71.2 -0.1 71.4	25.00 20.90 10.0 93.6 10.0 93.6	15.00 4.48 2.0 31.9 2.0 32.1
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv)	0.0 70.8 0.0 71.2 -0.1 71.4 -1.40	25.00 20.90 10.0 93.6 10.0 93.6	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Final Readings	0.0 70.8 0.0 71.2 -0.1 71.4 -1.40 893.00	25.00 20.90 10.0 93.6 10.0 93.6	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06 4.48
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Final Readings Zero Gas (chart %)	885 0.0 70.8 0.0 71.2 -0.1 71.4 -1.40 893.00	25.00 20.90 10.0 93.6 10.0 93.6 9.9 92.5 -0.03 20.62	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06 4.48
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Final Readings Zero Gas (chart %) Calibration Gas (chart %) Calibration Gas (chart %) Calibration Gas (chart %) Calibration Gas (chart %)	885 0.0 70.8 0.0 71.2 -0.1 71.4 -1.40 893.00 -0.1 69.8	25.00 20.90 10.0 93.6 10.0 93.6 9.9 92.5 -0.03 20.62	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06 4.48
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Final Readings Zero Gas (chart %) Calibration Gas (chart %) Calibration Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv)	885 0.0 70.8 0.0 71.2 -0.1 71.4 -1.40 893.00 -0.1 69.8 -1.40	25.00 20.90 10.0 93.6 10.0 93.6 9.9 92.5 -0.03 20.62	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06 4.48
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Final Readings Zero Gas (chart %) Calibration Gas (chart %) Calibration Gas (ppmv) Calibration Gas (ppmv) Calibration Gas (ppmv) Calibration Gas (ppmv)	885 0.0 70.8 0.0 71.2 -0.1 71.4 -1.40 893.00 -0.1 69.8	25.00 20.90 10.0 93.6 10.0 93.6 9.9 92.5 -0.03 20.62	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06 4.48
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Final Readings Zero Gas (chart %) Calibration Gas (chart %) Calibration Gas (ppmv) Calibration Gas (ppmv) Calibration Gas (ppmv) Bias and Drift Calculations	885 0.0 70.8 0.0 71.2 -0.1 71.4 -1.40 893.00 -0.1 69.8 -1.40 873.00	25.00 20.90 10.0 93.6 10.0 93.6 9.9 92.5 -0.03 20.62	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06 4.48 2.3 31.9 0.04 4.48
Analyzer Range (ppm), O₂ & CO₂ in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Final Readings Zero Gas (chart %) Calibration Gas (chart %) Calibration Gas (ppmv) Calibration Gas (ppmv) Calibration Gas (ppmv) Bias and Drift Calculations Zero Bias (% Chart) (Run-Direct Cal) ≤5%	885 0.0 70.8 0.0 71.2 -0.1 71.4 -1.40 893.00 -0.1 69.8 -1.40 873.00	25.00 20.90 10.0 93.6 10.0 93.6 9.9 92.5 -0.03 20.62 9.9 92.2 -0.03 20.55	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06 4.48 2.3 31.9 0.04 4.48
Analyzer Range (ppm), O, & CO₂ in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Calibration Gas (ppmv) Final Readings Zero Gas (chart %) Calibration Gas (ppmv) Final Readings Zero Gas (chart %) Calibration Gas (ppmv) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Calibration Gas (ppmv) Sero Gas (ppmv) Calibration Gas (ppmv) Calibration Gas (ppmv) Sias and Drift Calculations Zero Bias (% Chart) (Run-Direct Cal) ≤5% Calibration Bias (% Chart)	885 0.0 70.8 0.0 71.2 -0.1 71.4 -1.40 893.00 -0.1 69.8 -1.40 873.00	25.00 20.90 10.0 93.6 10.0 93.6 9.9 92.5 -0.03 20.62 9.9 92.2 -0.03 20.55	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06 4.48 2.3 31.9 0.04 4.48
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Final Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Bias and Drift Calculations Zero Bias (% Chart) (Run-Direct Cal) ≤5% Calibration Bias (% Chart) ≤5% Zero Drift (Chart %) (Run-Run) ≤3%	885 0.0 70.8 0.0 71.2 -0.1 71.4 -1.40 893.00 -0.1 69.8 -1.40 873.00 -0.1 -1.3 0.0	25.00 20.90 10.0 93.6 10.0 93.6 9.9 92.5 -0.03 20.62 9.9 92.2 -0.03 20.55	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06 4.48 2.3 31.9 0.04 4.48
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Final Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Bias and Drift Calculations Zero Bias (% Chart) (Run-Direct Cal) ≤5% Calibration Bias (% Chart) ≤5% Zero Drift (Chart %) (Run-Run) ≤3% Calibration Drift (Chart %)	885 0.0 70.8 0.0 71.2 -0.1 71.4 -1.40 893.00 -0.1 69.8 -1.40 873.00	25.00 20.90 10.0 93.6 10.0 93.6 9.9 92.5 -0.03 20.62 9.9 92.2 -0.03 20.55	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06 4.48 2.3 31.9 0.04 4.48
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Final Readings Zero Gas (chart %) Calibration Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Bias and Drift Calculations Zero Bias (% Chart) (Run-Direct Cal) ≤5% Calibration Bias (% Chart) ≤5% Zero Drift (Chart %) (Run-Run) ≤3% Calibration Drift (Chart %) ≤3% Run Results	885 0.0 70.8 0.0 71.2 -0.1 71.4 -1.40 893.00 -0.1 69.8 -1.40 873.00 -0.1 -1.3 0.0 1.6	25.00 20.90 10.0 93.6 10.0 93.6 9.9 92.5 -0.03 20.62 9.9 92.2 -0.03 20.55 -0.1 -1.4 0.0 0.3	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06 4.48 2.3 31.9 0.04 4.48 0.3 -0.3 0.1 0.0
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Final Readings Zero Gas (chart %) Calibration Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Bias and Drift Calculations Zero Bias (% Chart) (Run-Direct Cal) ≤5% Calibration Bias (% Chart) ≤5% Zero Drift (Chart %) (Run-Run) ≤3% Calibration Drift (Chart %) Run Results Raw Results (chart %)	885 0.0 70.8 0.0 71.2 -0.1 71.4 -1.40 893.00 -0.1 69.8 -1.40 873.00 -0.1 -1.3 0.0 1.6	25.00 20.90 10.0 93.6 10.0 93.6 9.9 92.5 -0.03 20.62 9.9 92.2 -0.03 20.55	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06 4.48 2.3 31.9 0.04 4.48 0.3 -0.3 0.1 0.0
Analyzer Range (ppm), O, & CO, in % Calibration Gas Certified Value (ppm or %) Strip Chart Offset Target Calibration Gas (Chart %) Actual Zero Gas from Direct (Chart %) Actual Calibration Gas from Direct (Chart %) Initial Readings Zero Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Final Readings Zero Gas (chart %) Calibration Gas (chart %) Calibration Gas (chart %) Zero Gas (ppmv) Calibration Gas (ppmv) Bias and Drift Calculations Zero Bias (% Chart) (Run-Direct Cal) ≤5% Calibration Bias (% Chart) ≤5% Zero Drift (Chart %) (Run-Run) ≤3% Calibration Drift (Chart %) ≤3% Run Results	885 0.0 70.8 0.0 71.2 -0.1 71.4 -1.40 893.00 -0.1 69.8 -1.40 873.00 -0.1 -1.3 0.0 1.6	25.00 20.90 10.0 93.6 10.0 93.6 9.9 92.5 -0.03 20.62 9.9 92.2 -0.03 20.55 -0.1 -1.4 0.0 0.3	15.00 4.48 2.0 31.9 2.0 32.1 2.4 31.9 0.06 4.48 2.3 31.9 0.04 4.48 0.3 -0.3 0.1 0.0

Testing by Cubix Corporation - Austin, Texas - Gainesville, Florida

Georgia-Pacific Palatka Operations, Bleach Plant Scrubber, Logged QA Calibration Records

Run 1	10/28/02	9:34:18	10:34:18					
Initial Linearity Test CO (ppmv) O2 (% vol) CO2 (% vol)	Zero I 0.33 0.00 0.00	244.64 4.50 4.52	20.90	11.95	0.12	0.00	-0.04	
Initial and Final Bias and Drift CO (ppmv) O2 (% vol) CO2 (% vol)	1-Zero 1 -2.97 -0.03 0.06	I-Span 887.15 11.77 7.94	-2.97	888.80 11.80	-0.20	-().()5 -0.6()	().()() ().08	S-Drift -0.13 -0.12 -0.27
Run Results and Cal Gases Used CO (ppmv) O2 (% vol) CO2 (% vol)	958.7 20.52 1.08	Corrected 955.3 20.76 1.04		4.53	20.90	11.94		
Run 2	10/28/02	11:27:39	12:27:39					
Initial Linearity Test CO (ppmv) O2 (% vol) CO2 (% vol)	Zero I 0.33 0.00 0.00	244.64 4.50 8.02		20.90	0.12	-(),()4	. 0.00	
Initial and Final Bias and Drift CO (ppmv) O2 (% vol) CO2 (% vol)	1-Zero I -2.97 -0.05 0.04	1-Span 888.80 20.70 4.50	-0.03	20.62	-().12	0.28 -1.12	-0.13 -0.08	S-Drift -0.34 0.32 0.13
Run Results and Cal Gases Used		Corrected	Ranges	Low Gas	Mid Gas	Span Gas		

Georgia-Pacific Palatka Operations, Bleach Plant Scrubber, Logged QA Calibration Records

Run 3	10/28/02 13	:17:44 PM I	14:17:44 PM					
Initial Linearity Test	Zero Lo	ow N	Mid	Span	L-Lin	M-Lin	S-Lin	
CO (ppmv)	0.33	244.64	430.65	889.46	0.67	0.83	-0.36	
O2 (% vol)	0.00	4.50	11.95	20.90	0.12	-0.04	0.00	
CO2 (% vol)	0.00	8.02	12.62	4.52	-0.20	0.00	-().27	
Initial and Final Bias and Drift	1-Zero I-S	Span F	F-Zero	F-Span	Z-Bias	S-Bias	Z-Drift	S-Drift
CO (ppmv)	-1.40	893.00	-1.40	873.00	-0.14	-1.32	0.00	1.60
O2 (% vol)	-0.03	20.62	-0.03	20.55	-0.12	-1.40	0.00	0.28
CO2 (% vol)	0.06	4.48	0.04	4.48	0.27	-0.27	0.13	0.00
Run Results and Cal Gases Used	Raw C	orrected	Ranges	Low Gas	Mid Gas	Span Gas		
CO (ppmv)	949.3	951.3	1250.0	253.0	441.0	885.0		
O2 (% vol)	20.38	20.69	25.00	4.53	11.94	20.90		
CO2 (% vol)	1.07	1.03	15.00	7.99	12.62	4.48		

Instrumental Analyses Quality Assurance Data

Date:

October 28, 2002

Company:

Georgia-Pacific Corporation

Facility:

Georgia-Pacific Palatka Operations Bleach Plany Wet Scrubber

Source ID:

Location:

Patatka, Putnam County, Florida

Technicians:

RPO, JTH

_	Instrumental Sample System Leak Checks						
Date	Run Vacuum Leak Rate Number (inches Hg) (inches Hg/min) Pass						
10/27/02	Set-Up	24.8	0.0	yes			
10/28/02	pre Run 1	24.0	0.0	yes			
10/28/02	post Run 3	24.2	0.0	yes			
Leak check crite	ria less than 1.0	" Hg Vac. Decli	ne at greater than 15.0	" Hg Vac.			

Continuous Emission Analyzer Interference Response Tests

Analyzer Interference Response Checks

(Frequency: Prior to initial use of sampling system or after alteration or modification.)

Test Date: September 27, 2002 Technician: RPO

Mobile Lab: T-13 Location: Gainesville, Florida

Analyzer	Manufacturer	Model	Serial Number	Detection Method/Comments
NO _x Analyzer	TECO	42C	42CHL-69541-363	Chemiluminescence with Ozone
CO Analyzer	TECO	48C	48C-70472-365	Infrared Absorption/GFC Detector
O ₂ Analyzer	Servomex	1440	1420C/2647	Paramagnetic Cell Detector
CO, Analyzer	Servomex	144()	01415/2537	Infrared Absorption/Solid State Detector
THC	California Analytical	300-HFID CE	4J11003	Flame Ionization Detector

Interferrent	Test Gases	Analyzer Response (ppmv or % as applicable)					
Type Gas	Conc.	NO_x	CO	O ₂	CO,	ТНС	
	!	0-25 ppmv	0-50 ppmv	0-25% vol	0-15% vol	0-100 ppmv	
CO/Methane in air	885/919	0.1 ppmv			0.00 %		
Propane in air	2000	0.1 ppmv	0.4 ppmv		0.03 %		
SO ₂ in N ₂	4400	0.2 ppmv	-0.3 ppmv	0.00 %	0.00 %	no data	
Air	dry instrument	< 0.1 ppmv	0.4 ppmv		0.03 %	no data	
Nitrogen	pre-purified	0.0 ppmv	0.3 ppmv	0.00 %	0.00 %	no data	
Air	UHC, CO free	0.0 ppmv	. 0.0 ppmv		0.01 %	no data	
CO ₂ / O ₂	4.54%/20.8%	< 0.1 ppmv	-0.2 ppmv			no data	
CO ₂ / O ₂	8.004%/11.91%	< 0.1 ppmv	-0.4 ppmv			no data	
CO ₂ / O ₂	12.62%/4.53%	< 0.1 ppmv	-0.6 ppmv	20 A		no data	
NO _x in N ₂	1209		0.4 ppmv	0.18 %	0.03 %	no data	

APPENDIX E: CALIBRATION CERTIFICATIONS



3434 Route 22 West • Branchburg, NJ 08876 USA Tel.: (908) 252-9300 • (800) 932-0624 • Fax (908) 252-0811 Shipped From: 80 Industrial Drive • Alpha, NJ 08865



CERTIFICATE OF ANALYSIS

EPA PROTOCOL MIXTURE

PROCEDURE #:

G1

CUSTOMER:

Cubix Corporation

CYLINDER #:

CC-94787

SGI ORDER #:

0016436

CYLINDER PRES:

2000 PSIG

ITEM#:

CGA OUTLET:

590

P.O.#:

2001032 T12 SID

CERTIFICATION DATE:

2/11/02

EXPIRATION DATE:

2/6/2005

CERTIFICATION HISTORY

	DATE OF	MEAN	CERTIFIED	ANALYTICAL
COMPONENT	ASSAY	CONCENTRATION	CONCENTRATION	ACCURACY
Carbon Monoxide	1/30/02	252.8 ppm	253 ppm	+/- 1%
	2/6/02	252.5 ppm		
Methane	2/11/02	249 ppm	249 ppm	+/- 1%
	 		-	

BALANCE

PREVIOUS CERTIFICATION DATES: None

REFERENCE STANDARDS

COMPONENT	SRM/NTRM#	CYLINDER#	CONCENTRATION
Carbon Monoxide	GMIS-1	CC94699	486 ppm
Methane	GMIS-1	CC52976	503.3 ppm

INSTRUMENTATION

COMPONENT	MAKE/MODEL	SERIAL #	DETECTOR	CALIBRATION
				DATE(S)
Carbon Monoxide	Horiba VIA-510	570423011	NDIR	1/8/02
Methane	H. Packard 6890	US00001434	GC - FID	2/5/02

THIS STANDARD IS NIST TRACEABLE. IT WAS CERTIFIED ACCORDING TO THE EPA PROTOCOL PROCEDURES. DO NOT USE THIS STANDARD IF THE CYLINDER PRESSURE IS LESS THAN 150 PSIG.

ANALYST:

DATE:

2/11/02

TED NEEME



3434 Route 22 West • Branchburg, NJ 08876 USA Tel.: (908) 252-9300 • (800) 932-0624 • Fax. (908) 252-0811 Shipped From: 80 Industrial Drive • Alpha, NJ 08865



CERTIFICATE OF ANALYSIS

EPA PROTOCOL MIXTURE

PROCEDURE #: G1

CUSTOMER:

Cubix Corporation

CYLINDER #:

SGI ORDER #:

0023960

CC-60135

CYLINDER PRES: 2000 PSIG

ITEM#:

P.O.#:

2002420

CGA OUTLET:

590

CERTIFICATION DATE: 7/19/2002 **EXPIRATION DATE:**

7/11/2005

CERTIFICATION HISTORY

DATE OF	MEAN	CERTIFIED	ANALYTICAL
ASSAY	CONCENTRATION	CONCENTRATION	ACCURACY
7/11/2002	441.6 ppm	441 ppm	+/- 1%
7/19/2002	439.9 ppm		•
7/11/2002	445 ppm	445 ppm	+/- 1%
,			
	ASSAY 7/11/2002 7/19/2002	ASSAY CONCENTRATION 7/11/2002 441.6 ppm 7/19/2002 439.9 ppm	ASSAY CONCENTRATION CONCENTRATION 7/11/2002 441.6 ppm 441 ppm 7/19/2002 439.9 ppm

BALANCE

PREVIOUS CERTIFICATION DATES: None

REFERENCE STANDARDS

THE BILLINGE OF THE BOTH TO	<u></u>		
COMPONENT	SRM/NTRM#	CYLINDER#	CONCENTRATION
Carbon Monoxide	NTRM-81681	CC-55779	994 ppm
Methane	GMIS-1	CC55777	993.6 ppm

INSTRUMENTATION

COMPONENT	MAKE/MODEL	SERIAL#	DETECTOR	CALIBRATION
· _				DATE(S)
Carbon Monoxide	Horiba VIA-510	570423011	NDIR	7/19/2002
Methane	H. Packard 6890	US00001434	GC - FID	6/24/2002

THIS STANDARD IS NIST TRACEABLE. IT WAS CERTIFIED ACCORDING TO THE EPA PROTOCOL PROCEDURES. DO NOT USE THIS STANDARD IF THE CYLINDER PRESSURE IS LESS THAN 150 PSIG.

ANALYST:

FRED PIKULA

DATE: 7/19/2002



3434 Route 22 West • Branchburg, NJ 08876 USA Tel.: (908) 252-9300 • (800) 932-0624 • Fax: (908) 252-0811 Shipped From: 80 Industrial Drive • Alpha, NJ 08865



CERTIFICATE OF ANALYSIS

EPA PROTOCOL MIXTURE

PROCEDURE #: G1

CUSTOMER:

Cubix Corporation

CYLINDER #:

CC126532

SGI ORDER #:

0000840

CYLINDER PRES: 2000 PSIG

ITEM#:

CGA OUTLET:

590

P.O.#:

G-1334

CERTIFICATION DATE: 1/31/2001 EXPIRATION DATE:

1/30/2004

CERTIFICATION HISTORY

	DATE OF	MEAN	CERTIFIED	ANALYTICAL
COMPONENT	ASSAY	CONCENTRATION	CONCENTRATION	ACCURACY
Carbon Monoxide	1/23/2001	885.2 ppm	885 ppm	+/- 1%
	1/31/2001	884.4 ppm		
Methane	1/30/2001	919 ppm	919 ppm	+/- 1%

BALANCE

Air

PREVIOUS CERTIFICATION DATES: None

REFERENCE STANDARDS

COMPONENT	SRM/NTRM#	CYLINDER#	CONCENTRATION
Carbon Monoxide	NTRM-81681	CC55721	994 ppm
Methane	GMIS-1	CC55777	994.1 ppm
		,	

INSTRUMENTATION

COMPONENT	MAKE/MODEL	SERIAL#	DETECTOR	CALIBRATION
				DATE(S)
Carbon Monoxide	Honba VIA-510	570423011	NDIR	1/19/2001
Methane	H. Packard 6890	US00001434	GC - FID	1/30/2001
				<u> </u>

THIS STANDARD IS NIST TRACEABLE. IT WAS CERTIFIED ACCORDING TO THE EPA PROTOCOL PROCEDURES. DO NOT USE THIS STANDARD IF THE CYLINDER PRESSURE IS LESS THAN 150 PSIG.

ANALYST:

DATE: 1/31/2001



3434 Route 22 West • Branchburg, NJ 08876 USA Tel.: (908) 252-9300 • (800) 932-0624 • Faz (908) 252-0611 Shipped From: 80 Industrial Drive • Alpha, NJ 08865



C	`F	R.	TΙ	F	ICA	١Т	F	റ	F	Α	N	ΑL	_Υ	'SI	S
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EPA PROTOCOL MIXTURE

PROCEDURE #: G1

CGA OUTLET:

CUSTOMER:

Cubix Corporation

CYLINDER #:

SGI ORDER #:

0021285

CC-133482

ITEM#:

CYLINDER PRES: 2000 PSIG

P.O.#:

2002275 T10LENO

Begin use 7/24/02

CERTIFICATION DATE: 5/24/2002 EXPIRATION DATE: 5/24/2005

CERTIFICATION HISTORY

	DATE OF	MEAN	CERTIFIED	ANALYTICAL
COMPONENT	ASSAY	CONCENTRATION	CONCENTRATION	ACCURACY
Carbon Dioxide	5/24/2002	4.48 %	4.48 %	+/- 1%
Oxygen	5/24/2002	20.9 %	20.9 %	+/- 1%

BALANCE

Nitrogen

PREVIOUS CERTIFICATION DATES: None

REFERENCE STANDARDS

COMPONENT	SRM/NTRM#	CYLINDER#	CONCENTRATION	
Carbon Dioxide	GMIS-1	CC-90832	9.98 %	
Oxygen	NTRM-1	CC-83909	22.8 %	

INSTRUMENTATION

COMPONENT	MAKE/MODEL	SERIAL#	DETECTOR	CALIBRATION
				DATE(S)
Carbon Dioxide	Horiba VIA-510	571417045	NDIR	5/24/2002
Oxygen	Horiba MPA-510	570694081	РМ	5/20/2002

THIS STANDARD IS NIST TRACEABLE. IT WAS CERTIFIED ACCORDING TO THE EPA PROTOCOL PROCEDURES. DO NOT USE THIS STANDARD IF THE CYLINDER PRESSURE IS LESS THAN 150 PSIG.

ANALYST:	0/.
•	EDED BIKLU V

DATE:	5/24/2002





3434 Route 22 West • Branchburg, NJ 08876 USA Tel:: (908) 252-9300 • (800) 932-0624 • Fax (908) 252-0811 Shipped From: 80 Industrial Drive • Alpha, NJ 08865

CERTIFICATE OF ANALYSIS

EPA PROTOCOL MIXTURE

PROCEDURE #: G1

CUSTOMER:

Cubix Corporation

CYLINDER #:

CC-127463

SGI ORDER #:

0023960

CYLINDER PRES: 2000 PSIG

ITEM#:

CGA OUTLET:

590

P.O.#:

2002420

CERTIFICATION DATE: 7/23/2002

EXPIRATION DATE:

7/23/2005

CERTIFICATION HISTORY

	DATE OF	MEAN	CERTIFIED	ANALYTICAL
COMPONENT	ASSAY	CONCENTRATION	CONCENTRATION	ACCURACY
Carbon Dioxide	7/23/2002	7.99 %	7.99 %	+/- 1%
Oxygen	7/23/2002	11.94 %	11.94 %	. +/- 1%
			·	

BALANCE

Nitrogen

PREVIOUS CERTIFICATION DATES: None

REFERENCE STANDARDS

COMPONENT	SRM/NTRM#	CYLINDER#	CONCENTRATION
Carbon Dioxide	GMIS-1	CC-90832	9.98 %
Oxygen	NTRM-1	CC-83909	22.8 %

INSTRUMENTATION

COMPONENT	MAKE/MODEL	SERIAL#	DETECTOR	CALIBRATION
				DATE(S)
Carbon Dioxide	Horiba VIA-510	571417045	NDIR	6/25/2002
Oxygen	Horiba MPA-510	570694081	PM	7/23/2002

THIS STANDARD IS NIST TRACEABLE. IT WAS CERTIFIED ACCORDING TO THE EPA PROTOCOL PROCEDURES. DO NOT USE THIS STANDARD IF THE CYLINDER PRESSURE IS LESS THAN 150 PSIG.

ANALYST:

DATE: 7/23/2002

RATA CLASS



Scott Specialty Gases

Dual-Analyzed Calibration Standard

9810 BAY AREA BLVD. PASADENA, TX 77507

Phone: 281-474-5800

Combination Commencer

Fax: 281-474-5857

CERTIFICATE OF ACCURACY: Interference Free Multi-Component EPA Protocol Gas

Assay Laboratory

P.O. No.:

G-1291

CUBIX CORPORATION

SCOTT SPECIALTY GASES

9810 BAY AREA BLVD PASADENA,TX 77507

Project No.: 04-85228-002

4536 NW 20TH DRIVE

GAINESVILLE FL



ANALYTICAL INFORMATION

This certification was performed according to EPA Traceability Protocol For Assay & Certification of Gaseous Calibration Standards;

Procedure #G1; September, 1997.

Cylinder Number:

ALM009152

Certification Date:

4/03/00

Customer

Exp. Date:

4/03/2003

Cylinder Pressure * * *: The same

1883 PSIG

ANALYTICAL

CERTIFIED CONCENTRATION (Moles)

12.62

ACCURACY ** +/-1%

TRACEABILITY

OXYGEN NITROGEN

COMPONENT

CARBON DIOXIDE

4.53 ፠ +/-1%

Direct NIST and NMi Direct NIST and NMi

7

BALANCE

Da not use when cylinder pressure is below 150 psig.

Analytical accuracy is based on the requirements of EPA Protocal procedure G1. September 1997.

Product certified as +/- 1% analytical accuracy is directly traceable to NIST or NMI standards

REFERENCE STANDARD

TYPE/SRM NO.

EXPIRATION DATE

CYLINDER NUMBER

CONCENTRATION

COMPONENT

NTRM

1/01/03 12/19/01

ALM042032 ALM031738 13.96 % 9.680 %

CO2/N2 OXYGEN

NTRM 2658 INSTRUMENTATION

INSTRUMENT/MODEL/SERIAL#

FTIR System/8220A/AAE9400260 MTJ-A/M200/171109

DATE LAST CALIBRATED

03/28/00

03/21/00

ANALYTICAL PRINCIPLE

Scott Enhanced FTIR GAS CHROMATOGRAPHY

ANALYZER READINGS

(Z = Zero Gas

R = Reference Gas T = Test Gas r = Correlation Coefficient)

First Triad Analysis

Second Triad Analysis

Calibration Curve

CARBON DIOXIDE

Date: 04/03/00 Response Unit: % R1 = 13.956 21 = 0.0220T1 = 12.629 R2 - 13.966 22 = 0.017872 = 12.617Z3 - 0.0276 R3 = 13.959 Avg. Concentration: 12.62

Concentration = A + Bx + Cx2 + Dx3 + Ex4 r = 0.999990 Constants: A = 0.000000B = 1.000000C = 0 000000 D = 0.000000 E = 0.000000

OXYGEN ::

Date:04/06/00 Resoonse Unit:AREA 21 = 114.00R1 a 35455 T1 = 16619. RZ = 35183. Z2 = 141.00T2 = 16552.

Z3 = 118.00 T3 = 16573. R3 = 35179. Avg. Concentration: 4.530

Concentration = A + Bx + Cx2 + Ox3 + Ex4(= 0.99999941B Constants: A = -0.034423978 = 0.000275952 C= E =

APPROVED BY:

Air Products and Chemicals, Inc.

5837 W. Filin Street Jacksonville, FL 32254 Telephone (904) 786-2663 FAX (904) 693-9128



30 March, 1995

Cubix Corporation 2106 NW 67th Place Suite 7 Gainesville, FL 32653

CERTIFICATE OF CONFORMANCE

This document certifies that the product listed below is supplied via Air Products and Chemicals. Inc. and complies with the current minimum purity specifications of Air Products and Chemicals, Inc., Specialty Gas Department.

Product

Hydrogen

Product Code

3602

Product

Oxygen

Product Code

1602

Shipper Number

854-C-78428

Product

Compressed Air

Product Code

9197

Product

Nitrogen

Product Code

2602

Shipper Number

854-C-78440

Authorized Signature

Dry Gas Meter Calibration

WORKING METER

Date: Prev. Calib. Date: 4/12/02 rebuilt

1 0000

Location: Technician: Meter Serial No: Cubix DGM ID rebuit
Cubix Austin Lab
Bradiey Rayhons
2962152
T-10

REFERENCE METER

 Calibration Date:
 4/11/02

 Location:
 Cubix Austin Lab

 Technician:
 Steve Oleyar

 Meter Serial No:
 F164240

 Cubix DGM ID
 American

 Calib. Factor (Y):
 1.0022

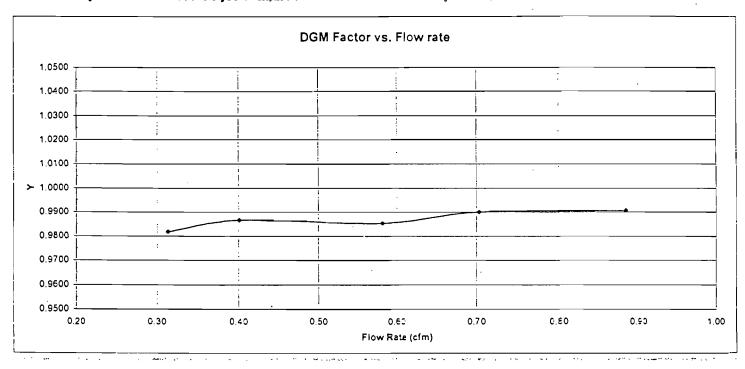
Prev. Calib Factor (Y):

REFERENCE M	ETER							Corr. Vol @
Calibration	Time	Start Temp	Stop Temp	Vol (initial)	Vol (final)	Vol. Total	Meter Rate	EPA STP
Run #	(min)	(deg F)	(deg F)	(cu ft)	(cu ft)	(cu ft)	(cu-ft /min)	(ದು ਜੈ)
1	20	74	73.7	18 936	25.078	6.155	0 3078	5.998
2	18	74	74.5	26.261	33.362	7.117	0.3954	6.928
3	10	74	73.4	12.401	18.122	5.734	0 5734	5.589
4	11	74	74.6	35.001	42.645	7.661	0.6965	7.453
5	11	7.5	75.1	44.308	53.922	9.635	0.8759	9.367

WORKING MET	rer							Corr. Vol @	Calculated		
Calibration	Time	Start Temp	Stop Temp	Vol (initial)	Vol (final)	Vol. Total	Meter Rate	EPA STP	DGM Factor	Dry Gas Meter (DGM Factor)	
Run#	(min)	(deg F)	· (deg F)	(cu ft)	(cu ft)	(cu ft)	(cu-ft /min)	(cu ft)	m	Calibration Test Results	
1	20	75	73.7	19.158	25.436	6.278	0.314	6.108	C.9819	* Average Y: 0.9869	
2	18	75	73.9	26.635	33.854	7.219	0,401	7.023	0.9866	Ave. Y w/in 5% of previous value:	YES
3	10	73	74.6	12.465	18.285	5.820	0.582	5.672	0.9854	Ave. Y between 0.95 and 1.05;	PASS
4	11	74	75.8	35.525	43.266	7.741	0.704	7.529	0.9900	Ind. Y values +/- 0.02 from Ave.:	PASS
5	11	76	73.9	44.957	54,684	9.727	0.854	9 455	0.9906		

Criteria:

^{*} Y- ratio of the reading of the reference meter to the working DGM. Acceptable tolerance of individual values from the average is +/- 0.02, with a value between 0.95 and 1.05.



Suche Rahman

Pitot Tube Calibration Sheet

S-Type Tip Inspection (Method 2, Section 4)

Alignment Inspection

74

Transverse tube axis pitot-tip angle:

$$\alpha_1 = 4$$
 °

$$\alpha_2 = 3$$

Each α must be less than 10° from perpendicular to the transverse tube axis

Longitudinal tube axis pitot-tip angle:

$$\beta_1 = \mathcal{Q}$$
 °

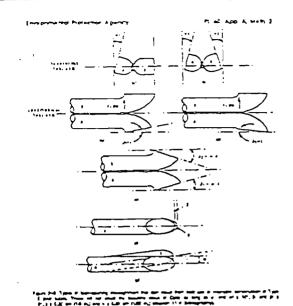
$$\beta_1 = 3$$
 °

Each β must be less than 5° from partallel to the longitudinal tube axis

Pitot-tip end length alignment:

$$z = \bigcirc (in) \text{or cm}$$

Z must be ≤ 0.32 cm (1/8 in)



Pitot-tip centriod alignment with respect to transverse axis:

$$w = 0$$
 (in or \widehat{m})

PL MC ADC. A. MAPPL 2

W must be ≤ 0.08 cm (1/32 in)

Pitot Tip Dimension Check

External tubing diameter:

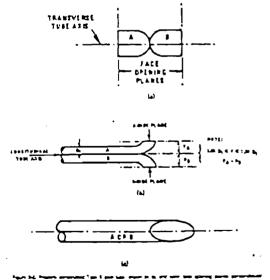
$$D_i = .375$$
 (in or cm)

D, must be between 0.48 and 0.95 cm (3/16 and 3/8 in)

Base to opening plane distance:

$$P_{A} = P_{B} = .475$$
 (in) or cm

 P_A and P_B must be between 1.05 D, and 1.50 D,



light (A), Property properties ² pp. 2 pp. 14th proper (t. 6), price unto the operand process proceedings.

§ Transmiss (MS) (B) (S) are upon the process proper properties of (s) are not for (s) are made of (s) are not of (s) are not of (s) are not of (s) are not of (s) are not (

Pitot Tube Coefficient

 $C_p = 0.84$

Pitot Tube: 2110

Date and Initials: 8-7-02



ALTIMETER TEST RECORD

This unit was tested and inspected IAW FAR Part 43, Appendix E, and is approved for return to service.

DATE:	3-	8-	02
-------	----	----	----

WORK ORDER #: 350/

SCALE ERROR

oches simon
-100015
o Ø :
+ 500
+1000 + 10
+1500
+2000 +10
+3000 +5
+4000
+60005
+8000 <u>+5</u>
+10,000 <u>+ 15</u>
+12.000 + 26
+14,000
+16,000 _ + 15
+18.000
+20,000/
+22.000
+25,000
+30,000
+35,000
+40,000
+45,000
+50,000 /
2n 1
START PRESSURE
FINAL PRESSURE 30-06

BAROMETRIC SCALE ERROR TEST

28.10	30.50 _ 30.90 _	+ <u>5</u>
29.00	30.99	Ø
29.50 <u>Ø.</u> 29.92 <u>Ø</u>		

FRICTION TEST

1000 <u>30</u>	20.000
2000 <u>30</u>	25.000
3000 <u>30</u>	30,000
5000 30	35.000
10,000 <u>'40 </u>	40.000
15.000 45	50,000

CASE LEAK TEST @ 18,000	\sim
CASE LEAK TEST @ 1,200	Ø

HYSTERESIS TEST @ 50%_	20
HYSTERESIS TEST @ 40%_	15

		15	
AFTER	EFFECT	/ン	

SERIAL NUMBER		124
INSPECTOR /	1 HOLK	<i>[</i> ,
	\mathcal{I}	0

TRAILER 10 ALTIMETER/BAROMETER CALIBRATION SHEET

3FG/C 9001

BFGoodrich

Aerospace

817 Dessau Road Austin, Texas 78753 512-251-3441 FAX 512-990-1271

Component Overhaul & Repair

FAA Repair Station No. UZ2R232L

CASTLEBERRY AERCOR

Serviceable Part Tag

:	COMPONENT Altimeter PART NO 5934P-11, SERIAL NO J 5924 MFG United Faste. WO	83 rk order # <u>V 70 7/</u>
	🖾 Overhaul 🔲 Repair 🗀 Bench Check	& Test
	The Aircraft Appliance identified above bench tested (as per block marked) and current Federal Aviation Administration Rereturn to service. Details of this component	inspected, in accordance with— egulations, and is approved for
	QIDBIT	JAN 16 1995
	AUTHORIZED SIGNATURE	DATE

	ALTIMETER SCALE ERROR						
PART NO	PART NO. 5934 PIA83 SERIAL NO. J5924						
		ALTI	TETER PRESSURE				
PT (FT)	DEDICATOR READ- THGS AT + 25°C	PI (FI)			INDICATOR READ- INGS AT + 25 ° C		
-1000	+5	8,000	÷ 5	30,000			
۰۰	0	10,000	÷ 10	35,000			
5∞	Ô	12,000	+ 15	40,000			
1000	U	14,000	+ 15	45,000	!		
1500	0	16,000	+5	50,000			
2000	Ð	18,000	0	55,000			
3000	- 5	20,000	5	60,000			
4000	~ / · ·	22,000		70,000			
6000	7/5	25,000		80,000			

BFG C9102

Best Available Copy

NIST CALIBRATION CERTIFICATE

Page 2 of 2

Catalog Number:

17005-00

Certificate Reference Number 3924899

Instrument Tolerance

	-	-		±3% full-s	cale				
	Equipn	nent "As	Found"			quip	ment "A	s Left"	
	Test Points	Reading	Deviation	0.0.T		Points '	Reading	Deviation	
Measured	17.276	學學製質	10 HERO		清 数	S113	(W)	《表題事的	1
in:	32.00	32.0	0.0000		,	32.00	32.0	0.0000	
°F	110.00	110.0	0.0000			10.00	110.0	0.000	
Measured							Z Dr		_
in:	32.00	32.0	0.0000			32.00	32.0	0.0000	
°F	32.00	32.0	0.0000			ing:	20.00E	1500000	_
	110.00	110.0	0.0000	<u></u>	11	10.00	110.0	0.0000	
Measured in:									1
					1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1				j
Measured in:									1
							遊戲物		j
Measured in:									
		秦金 湯	图 基 图 图 图 图 图 图 图 图 图 图 图 图 图 图 图 图 图 图						I
	Note the	Chack	under the C () T oo!	indicates the an	uin-s-	at in Oct Of	Tolorares	
					indicates the equal lab conditions of				9. 5 "Hg
	_		i inc dimate	Sim oned	ias conditoris 0	••		Jo /oiCi Z	J.J ng
Additional n/a	comments	:							



625 East Bunker Court, Vernon Hills, Illinois, 60061 Domestic 866-InnoCal - Fax 847-247-2984

NIST CALIBRATION CERTIFICATE

Page 1 of 2

Catalog Number:

17005-00

Certificate Reference Number 3924899

Unit Under Test 1:

03312-20

Unit Under Test 2:

n/a

Serial Number 1:

57778

Serial Number 2:

n/a

Certificate Completed for: Cubix Corp

3709 SW 42nd Ave

Gainsville

FL

32608

InnoCal certifies that the calibration of the listed units, used procedure number MWI-17005-00 with equipment traceable to the National Institute of Standards and Technology (NIST), and the test was performed in accordance with ANSI/NCSL Z540-1,ISO Guide 25.

Best measurement uncertainty: k=2, ±0.08°C

Listed uncertainties represent the best measurement uncertainty expressed at 95% confidence level. Actual uncertainties available upon request.

Purchase Order Number:

2002615

Secondary ID #: n/a

Equipment Condition: USED

Calib	ration	Stai	つべつア	de i	604
Callb	auon	Stail	iuai i	us c	ocu.

Manufacturer

Function Performed

Model Number

Serial Number

Due Date

Hart Scientific

Platinum Resistance Probe

5680

1074

04/14/03

Ertco/Hart

Temperature Indicator

850

85307

04/14/03

Lab Technician: 321

Date Completed: 10/17/02

Received Date 9/18/02



One Omega Drive, Box 4047, Stamford, CT 06907 (203) 359-1660 - http://www.omega.com - e-mail: info@omega.com

CERTIFICATE OF CALIBRATION

Model HH-25KF Serial Number 7- 233418

Omega Engineering, Inc., certifies that the above listed instrument has been calibrated using standards whose accuracy is traceable to the U.S. National Institute of Standards and Technology, and meets or exceeds its published specifications. Calibration traceability of the above listed instrument is in full compliance with ANSI/Z540-1-1994 standards and requirements.

DATE

RF

TESTED BY

AUTHORIZED SIGNATURE

MD-4 ©Copyright 1998 Omega Engineering, Inc.

Placed in service: August 14,2002 Recalibration Date: February 1,2003 Location: Trailer 10



Certificate Of Calibration

CUBIX

Cust. P.O. #:

G1342

Report #:

102915471

Test Item:

ASTM-1C-CC

Test Date:

22-FEB-01

Serial #:

99293

Recal Date: Per System Application

Omega Engineering; Inc. certifies that the above instrumentation has been calibrated and tested to meet or exceed the published specifications. This calibration and testing was performed using instrumentation and standards that are traceable to the United States National Institute of Standards and Technology. Calibration on this product was performed by an approved Supplier/ Lab of Omega Engineering, Inc. and is in compliance with MIL-STD-45662A.

Test Conditions:

Temperature

22 C

Relative Humidity

35%

NIST Traceable Test Numbers:

213426,264615-01

Temperature	Thermometer Reading	Correction
	We certify that subject thermometer conforms to specifications and tolerances stated in A.S.T.M. Designate E-1, Table 1, No. 1C, Scale Error + or - 0.5 C Max.	

Metrology Inspector

27-FEB-01

APPENDIX F: LOGGED DATA RECORDS 1-MINUTE AVERAGES

	-	!	CO	O2	CO2	AVE CO	AVE O2	AVE CO2
Run Number	Date	Time	(ppmv)	(% vol)	(% vol)	(ppmv)	(% vol)	(% vol)
START Run I	10/28/02	9:34:18	843.3	20.60	0.88	843.3	20.60	0.88
Run 1	10/28/02	9:35:18	850.0	20.58	0.94	846.6	20.60	0.91
Run I	10/28/02	9:36:18	841.2	20.60	0.94	844.8	20.60	0.92
Run I	10/28/02	9:37:18	910.5	20.60	0.96	861.2	20.60	0.93
Run 1	10/28/02	9:38:18	853.2	20.60	0.96	859.6	20.60	0.94
Run 1	10/28/02	9:39:18	895.1	20.60	0.94	865.5	20.60	0.95
Run 1	10/28/02	9:40:18	910.5	20.60	1.00	871.9	20.60	0.95
Run 1	10/28/02	9:41:18	856.6	20.58	0.96	870.0	20.60	0.95
Run I	10/28/02	9:42:18	909.4	20.58	0.94	874.4	20.60	0.95
Run 1	10/28/02	9:43:18	851.1	20.58	0.94	872.0	20.59	0.94
Run 1	10/28/02	9:44:18	833.5	20.58	0.90	868.5	20.59	0.94
Run 1	10/28/02	9:45:18	908.3	20.58	0.92	871.9	20.59	0.94
Run 1	10/28/02	9:46:18	868.7	20.55	0.98	871.6	20.59	0.94
Run 1	10/28/02	9:47:18	930.3	20.53	1.00	875.8	20.59	0.94
Run I	10/28/02	9:48:17	869.8	20.53	1.02	875.4	20.58	0.94
Run 1	10/28/02	9:49:16	919.3	20.55	1.04	878.1	20.58	0.95
Run 1	10/28/02	9:50:18	953.4	20.55	1.06	882.6	20.58	0.96
Run 1	10/28/02	9:51:17	892.9	20.55	1.04	883.1	20.58	0.96
Run I	10/28/02	9:52:18	944.6	20.55	1.04	886.4	20.57	0.96
Run 1	10/28/02	9:53:17	928.1	20.58	1.06	888.4	20.57	0.97
Run 1	10/28/02	9:54:17	961.1	20.53	1.08	891.9	20.57	0.97
Run 1	10/28/02	9:55:17	963.3	20.53	1.12	895.2	20.57	- 0.98
Run 1	10/28/02	9:56:18	985.5	20.53	1.12	899.1	20.57	0.99
Run 1	10/28/02	9:57:18	961.1	20.55	1.14	901.7	20.57	0.99
Run 1	10/28/02	9:58:18	1000.7	20.58	1.12	905.6	20.57	1.00
Run 1	10/28/02	9:59:18	999.6	20.55	1.16	909.2	20.57	1.00
Run 1	10/28/02	10:00:18	1015.4	20.58	1.08	913.2	20.57	1.01
Run I	10/28/02	10:01:18	997.4	20.55	1.08	916.2	20.57	1.01
Run 1	10/28/02	10:02:18	964.4	20.55	1.04	917.8	20.57	1.01
Run I	10/28/02	10:03:18	1000.7	20.55	1.06	920.6	20.57	1.01
Run 1	10/28/02	10:04:18	975.4	20.53	1.10	922.4	20.56	1.02
Run I	10/28/02	10:05:18	995.8	20.53	1.08	924.7	20.56	1.02
Run 1	10/28/02	10:06:18	954.5	20.53	1.06	925.6	20.56	1.02

			CO	O2	CO2	AVE CO	AVE O2	AVE CO2
Run Number	Date	Time	(ppmv)	(% vol)	(% vol)	(ppmv)	(% vol)	(% vol)
Run 1	10/28/02	10:07:18	987.5	20.53	1.06	927.4	20.56	1.02
Run 1	10/28/02	10:08:18	930.3	20.50	1.06	927.5	20.56	1.02
Run 1	10/28/02	10:09:18	987.5	20.53	1.02	929.1	20.56	1.02
Run 1	10/28/02	10:10:18	949.0	20.50	1.08	929.7	20.56	1.02
Run 1	10/28/02	10:11:18	1000.7	20.50	1.08	931.5	20.56	1.02 -
Run 1	10/28/02	10:12:18	1015.0	20.48	1.10	933.7	20.55	1.03
Run I	10/28/02	10:13:17	1021.3	20.45	1.10	935.9	20.55	1.03
Run 1	10/28/02	10:14:17	1003.2	20.45	1.16	937.5	20.55	1.03
Run 1	10/28/02	10:15:17	1000.7	20.45	1.16	939.0	20.55	1.03
Run I	10/28/02	10:16:17	1003.0	20.45	1.18	940.5	20.55	1.04
Run 1	10/28/02	10:17:17	1005.7	20.45	1.22	942.0	20.54	1.04
Run 1	10/28/02	10:18:17	1015.7	20.45	1.18	943.6	20.54	1.04
Run I	10/28/02	10:19:17	1008.7	20.45	1.18	945.0	20.54	1.05
Run 1	10/28/02	10:20:17	1002.7	20.48	1.18	946.3	20.54	1.05
Run' I	10/28/02	10:21:17	947.9	20.45	1.10	946.3	20.54	1.05
Run 1	10/28/02	10:22:17	990.7	20.40	1.16	947.2	20.53	1.05
Run 1	10/28/02	10:23:17	990.1	20.43	1.18	948.1	20.53	1.05
Run I	10/28/02	10:24:17	1000.3	20.50	1.16	949.1	20.53	1.06
Run 1	10/28/02	10:25:17	1024.1	20.53	1.10	950.5	20.53	1.06
Run 1	10/28/02	10:26:17	1035.3	20.50	1.16	952.1	20.53	1.06
Run I	10/28/02	10:27:17	1007.3	20.50	1.16	953.1	20.53	1.06
Run I	10/28/02	10:28:17	1002.0	20.50	1.18	954.0	20.53	. 1.06
Run 1	10/28/02	10:29:17	1012.8	20.50	1.22	955.1	20.53	1.06
Run 1	10/28/02	10:30:17	998.6	20.50	1.24	955.8	20.53	1.07
Run I	10/28/02	10:31:17	987.5	20.48	1.28	956.4	20.53	1.07
Run 1	10/28/02	10:32:17	999.6	20.45	1.26	957.1	20.53	1.07
Run 1	10/28/02	10:33:17	1000.7	20.43	1.28	957.8	20.52	1.08
END Run I	10/28/02	10:34:17	1012.4	20.43	1.32	958.7	20.52	1.08

	1	!	CO	. O2	CO2	AVE CO	AVE O2	AVE CO2
Run Number	Date	Time	(ppmv)	(% vol)	(% vol)	(ppmv)	(% vol)	(% vol)
START Run 2	10/28/02	11:27:40	1012.8	20.43	1.32	1012.8	20.43	1.32
Run 2	10/28/02	11:28:40	1000.8	20.45	1.28	1034.6	20.44	1.31
Run 2	10/28/02	11:29:39	1043.0	20.45	1.32	1020.5	20.43	1.32
Run 2	10/28/02	11:30:39	1022.8	20.43	1.32	1020.2	20.44	1.31
Run 2	10/28/02	11:31:39	1047.0	20.43	1.34	1027.8	20.43	1.32
Run 2	10/28/02	11:32:39	1105.0	20.45	1.30	1034.8	20.43	1.32
Run 2	10/28/02	11:33:39	1049.0	20.48	1.30	1041.2	20.43	1.32
Run 2	10/28/02	11:34:39	788.8	20.30	1.22	1040.1	20.44	1.29
Run 2	10/28/02	11:35:39	1063.0	20.40	1.28	1030.5	20.43	1.29
Run 2	10/28/02	11:36:39	1022.8	20.43	1.26	1033.0	20.43	1.29
Run 2	10/28/02	11:37:39	1071.0	20.43	1.28	1034.2	20.43	1.29
Run 2	10/28/02	[11:38:39	1089.0	20.45	1.32	1036.9	20.43	1.29
Run 2	10/28/02	11:39:39	1041.0	20.45	1.30	1042.5	20.43	1.29
Run 2	10/28/02	11:40:39	1107.0	20.48	. 1.30	1044.7	20.43	1.29
Run 2	10/28/02	11:41:39	1051.0	20.43	1.32	1045.3	20.43	1.29
Run 2	10/28/02	11:42:39	1057.0	20.45	1.30	1047.6	20.43	1.29
Run 2	10/28/02	11:43:39	1087.0	20.43	1.30	1048.9	20.43	1.29
Run 2	10/28/02	11:44:39	1092.8	20.45	1.30	1050.3	20.43	1.29
Run 2	10/28/02	11:45:39	1069.0	20.43	1.28	1053.1	20.43	1.29
Run 2	10/28/02	11:46:39	1083.0	20.40	1.32	1053.8	20.43	1.29
Run 2	10/28/02	11:47:39	1081.0	20.40	1.30	1055.6	20.43	. 1.29
Run 2	10/28/02	11:48:39	1083.0	20.43	1.28	1057.1	20.43	- 1.29
Run 2	10/28/02	11:49:39	1047.0	20.53	0.78	1057.6	20.43	1.29
Run 2	10/28/02	11:50:39	1061.0	20.40	1.26	1052.9	20.43	1.28
Run 2	10/28/02	11:51:39	1123.0	20.40	1.32	1054.3	20.43	1.28
Run 2	10/28/02	11:52:39	1081.0	20.43	1.24	1057.3	20.43	1.28
Run 2	10/28/02	11:53:39	1127.0	20.43	1.24	1058.8	20.43	1.28
Run 2	10/28/02	11:54:39	1061.0	20.43	1.26	1059.3	20.43	1.28
Run 2	10/28/02	11:55:39	1076.8	20.45	1.22	1060.3	20.43	1.28
Run 2	10/28/02	11:56:39	1127.0	20.40	1.30	1061.0	20.43	1.28
Run 2	10/28/02	11:57:39	1097.0	20.43	1.28	1063.2	20.43	1.28
Run 2	10/28/02	11:58:39	1127.0	20.43	1.28	1064.7	20.43	1.28
Run 2	10/28/02	11:59:39	1081.0	20.43	1.30	1065.7	20.43	1.28

	-	!	CO	O2	CO2	A VE CO	AVE O2	AVE CO2
Run Number	Date	Time	(ppmv)	(% vol)	(% vol)	(ppmv)	(% vol)	(% vol)
Run 2	10/28/02	12:00:39	1095.0	20.45	1.30	1066.8	20.43	1.28
Run 2	10/28/02	12:01:39	1079.0	20.43	1.26	1067.1	20.43	1.28
Run 2	10/28/02	12:02:39	1093.0	20.45	1.28	1067.8	20.43	1.28
Run 2	10/28/02	12:03:39	1087.0	20.45	1.30	1067.8	20.43	1.28
Run 2	10/28/02	12:04:39	0.1011	20.40	1.28	1069.0	20.43	1.28
Run 2	10/28/02	12:05:39	1149.0	20.43	1.30	1070.3	20.43	1.28
Run 2	10/28/02	12:06:39	1145.0	20.38	1.28	1072.7	20.43	1.28
Run 2	10/28/02	12:07:39	1209.0	20.38	1.32	1075.0	20.43	1.28
Run 2	10/28/02	12:08:39	1171.0	20.40	1.32	1077.7	20.43	1.28
Run 2	10/28/02	12:09:39	1187.0	20.40	1.32	1079.9	20.43	1.28
Run 2	10/28/02	12:10:39	1109.0	20.43	1.28	1081.8	20.43	1.28
Run 2	10/28/02	12:11:39	1131.0	20.43	1.22	1082.9	20.43	1.28
Run 2	10/28/02	12:12:39	1125.0	20.70	1.20	1083.4	20.43	1.28
Run 2	10/28/02	12:13:39	1099.0	20.48	1.16	1083.3	20.43	1.28
Run 2	10/28/02	12:14:39	1125.0	20.45	1.20	1083.4	20.43	1.28
Run 2	10/28/02	12:15:39	1091.0	20.48	1.18	1084.1	20.43	1.28
Run 2	10/28/02	12:16:39	1135.0	20.48	1.20	1084.5	20.43	1.27
Run 2	10/28/02	12:17:39	1083.0	20.48	1.18	1085.0	20.43	1.27
Run 2	10/28/02	12:18:39	1127.0	20.45	1.18	1085.8	20.43	1.27
Run 2	10/28/02	12:19:38	1113.0	20.45	1.20	1086.0	20.43	1.27
Run 2	10/28/02	12:20:38	1079.0	20.45	1.20	1086.5	20.43	. 1.27
Run 2	10/28/02	12:21:38	1145.0	20.45	1.20	1087.0	20.43	- 1.27
Run 2	10/28/02	12:22:38	1153.0	20.45	1.20	1087.6	20.43	1.27
Run 2	10/28/02	12:23:38	1091.0	20.43	1.22	1088.5	20.43	1.26
Run 2	10/28/02	12:24:38	1113.0	20.45	1.16	1089.4	20.43	1.26
Run 2	10/28/02	12:25:38	1173.0	20.45	1.20	1089.7	20.43	1.26
Run 2	10/28/02	12:26:38	1127.0	20.45	1.20	1090.3	20.43	1.26
END Run 2	10/28/02	12:27:38	1137.0	20.40	1.26	1091.3	20.43	1.26

	İ		· CO	· O2	CO2	AVE CO	AVE O2	AVE CO2
Run Number	Date	Time	(ppmv)	(% vol)	(% vol)	(ppmv)	(% vol)	(% vol)
START Run 3	10/28/02	13:17:45	1009.0	20.40	1.04	1009.0	20.40	1.04
Run 3	10/28/02	13:18:45	1023.0	20.45	1.06	1004.8	20.42	1.06
Run 3	10/28/02	13:19:45	969.0	20.45	1.04	999.4	20.44	1.04
Run 3	10/28/02	13:20:45	991.0	20.45	1.00	996.6	20.43	1.04
Run 3	10/28/02	13:21:45	983.0	20.45	0.98	992.1	20.44	1.03
Run 3	10/28/02	13:22:45	979.0	20.43	1.02	991.8	20.44	1.02
Run 3	10/28/02	13:23:45	991.0	20.43	1.02	988.9	20.44	1.02
Run 3	10/28/02	13:24:45	957.0	20.43	1.02	987.7	20.44	1.02
Run 3	10/28/02	13:25:45	1007.0	20.43	1.06	986.4	20.43	1.02
Run 3	10/28/02	13:26:45	923.0	20.28	1.04	985.4	20.42	1.02
Run 3	10/28/02	13:27:45	1015.0	20.33	1.04	985.1	20.41	1.03
Run 3	10/28/02	13:28:45	1025.0	20.33	1.14	986.6	20.40	1.03
Run 3	10/28/02	13:29:45	1039.0	20.38	1.12	992.9	20.40	1.04
Run 3	10/28/02	13:30:45	1089.0	20.38	1.12	997.1	20.40	1.05
Run 3	10/28/02	13:31:45	1055.0	20.38	1.14	1002.2	20.39	1.06
Run 3	10/28/02	13:32:45	1093.0	20.38	1.12	1007.8	20.39	1.06
Run 3	10/28/02	13:33:45	1065.0	20.35	1.14	1010.7	20.39	1.07
Run 3	10/28/02	13:34:44	1015.0	20.35	1.10	1014.0	20.39	1.07
Run 3	10/28/02	13:35:44	1083.0	20.35	1.14	1015.7	20.38	1.07
Run 3	10/28/02	13:36:44	1007.0	20.35	1.14	1017.6	20.38	1.07
Run 3	10/28/02	13:37:44	1013.0	20.38	1.08	1018.3	20.38	1.08
Run 3	10/28/02	13:38:44	1025.0	20.35	1.14	1017.1	20.38	1.08
Run 3	10/28/02	13:39:44	1005.0	20.35	1.12	1017.4	20.38	1.08
Run 3	10/28/02	13:40:44	1037.0	20.33	1.12	1016.7	20.38	1.08
Run 3	10/28/02	13:41:44	993.0	20.33	1.14	1016.6	20.38	1.09
Run 3	10/28/02	13:42:44	999.0	20.33	1.12	1016.1	20.37	1.09
Run 3	10/28/02	13:43:44	947.0	20.43	1.14	1013.9	20.37	1.09
Run 3	10/28/02	13:44:44	937.0	20.38	1.12	1011.8	20.38	1.09
Run 3	10/28/02	13:45:44	935.0	20.40	1.10	1008.9	20.38	1.09
Run 3	10/28/02	13:46:44	911.0	20.40	1.08	1006.3	20.38	1.09
Run 3	10/28/02	13:47:44	959.0	20.40	1.12	1003.6	20.38	1.09
Run 3	10/28/02	13:48:44	945.0	20.40	1.14	1001.9	20.38	1.09
Run 3	10/28/02	13:49:44	971.0	20.40	1.10	1000.9	20.38	1.09

		-	CO	O2	CO2	AVE CO	AVE O2	AVE CO2
Run Number	Date	Time	(ppmv)	(% vol)	(% vol)	(ppmv)	(% vol)	(% vol)
Run 3	10/28/02	13:50:44	961.0	20.38	1.16	999.0	20.38	1.10
Run 3	10/28/02	13:51:44	929.0	20.35	1.08	998.1	20.38	1.10
Run 3	10/28/02	13:52:44	973.0	20.35	1.08	996.5	20.38	1.10
Run 3	10/28/02	13:53:44	909.0	20.38	1.12	994.6	20.38	1.10
Run 3	10/28/02	13:54:44	945.0	20.33	1.06	993.4	20.38	1.09
Run 3	10/28/02	13:55:44	933.0	20.33	1.08	991.5	20.38	1.09
Run 3	10/28/02	13:56:44	690.8	20.35	0.98	988.5	20.38	1.09
Run 3	10/28/02	13:57:44	927.0	20.33	1.04	984.3	20.37	1.09
Run 3	10/28/02	13:58:44	873.0	20.35	1.00	982.1	20.37	1.09
Run 3	10/28/02	13:59:44	891.0	20.38	1.02	980.0	20.37	1.08
Run 3	10/28/02	14:00:44	915.0	20.38	1.06	977.9	20.37	1.08
Run 3	10/28/02	14:01:44	861.0	20.38	1.04	976.3	20.37	1.08
Run 3	10/28/02	14:02:44	921.0	20.40	1.06	974.2	20.37	1.08
Run 3	10/28/02	14:03:44	855.0	20.38	1.06	972.2	20.37	1.08
Run 3	10/28/02	14:04:44	893.0	20.38	1.02	970.4	20.37	1.08
Run 3	10/28/02	14:05:44	849.0	20.38	1.04	967.8	20.37	1.08
Run 3	10/28/02	14:06:44	889.0	20.40	1.04	966.3	20.37	1.08
Run 3	10/28/02	14:07:44	917.0	20.40	1.04	964.7	20.37	1.08
Run 3	10/28/02	14:08:44	879.0	20.40	1.06	963.3	20.37	1.08
Run 3	10/28/02	14:09:44	903.0	20.38	1.04	962.1	20.37	1.08
Run 3	10/28/02	14:10:44	863.0	20.38	1.08	960.2	20.38	1.08
Run 3	10/28/02	14:11:44	855.0	20.38	1.02	958.7	20.38	- 1.08
Run 3	10/28/02	14:12:44	917.0	20.38	1.06	957.2	20.38	1.07
Run 3	10/28/02	14:13:44	879.0	20.38	1.06	956.0	20.38	1.07
Run 3	10/28/02	14:14:44	845.0	20.40	0.96	954.6	20.38	1.07
Run 3	10/28/02	14:15:44	883.0	20.38	0.98	952.6	20.38	1.07
Run 3	10/28/02	14:16:44	825.0	20.38	0.96	951.0	20.38	1.07
END Run 3	10/28/02	14:17:44	849.0	20.38	0.90	949.3	20.38	1.07