

REPORT ON MERCURY TESTING

**WHEELABRATOR NORTH BROWARD, INC.
UNIT 3 FF OUTLET
POMPANO BEACH, FL**

**CLEANAIR PROJECT No: 10955-7
REVISION 0: JANUARY 6, 2011**



Wheelabrator North Broward Inc.

A Waste Management Company

2600 N.W. 48th Street
Pompano Beach, FL 33073

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BUREAU OF
AIR REGULATION

January 10, 2011

CERTIFIED MAIL #70031010000154667654

Mr. Lennon Anderson
Air Program Administrator
Florida Department of Environmental Protection
Southeast District
400 North Congress Ave., Suite 200
West Palm Beach, FL 33401

Re: Wheelabrator North Broward
F.A.C. 62-296.416 Quarterly Mercury Stack Testing
Fourth Quarter of 2010, Report Submittal

Dear Mr. Anderson:

As required by F.A.C. 62-296.416, please find enclosed the 2010 fourth quarter report on mercury stack testing which was conducted on Unit #3.

I, the undersigned, am a responsible official, as defined in Rule 62-210.200, F.A.C., of the Title V source addressed in this submittal. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements and information in this document are true, accurate and complete.

If there are any questions, please contact this office at (954) 971-8701.

Sincerely,

Jim Epsilantis
Acting Plant Manager

cc: USEPA, Region IV, Pesticides and Toxics Management Division, Air & EPCRA Enforcement
Branch, Air Enforcement Section CERTIFIED MAIL #70031010000154667661
FDEP, Tallahassee, Bureau of Air Regulation, New Source Review Section,
CERTIFIED MAIL #70031010000154667678
Broward County Department of Planning and Environmental Protection, Air Quality Division
CERTIFIED MAIL #70031010000154667685

Chuck Faller (with)
Tim Porter (without)
Rob French - MPI - (with)





Wheelabrator North Broward, Inc.
2600 NW 48th Street
Pompano Beach, FL 33073

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REPORT ON MERCURY TESTING

Performed for:
WHEELABRATOR NORTH BROWARD, INC.
UNIT 3 FF OUTLET
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-7
Revision 0: January 6, 2011

To the best of our knowledge, the data presented in this report are accurate, complete, error free, legible and representative of the actual emissions during the test program.

Prepared by,



Scott Brown
Project Manager
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Reviewed by,



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REVISION HISTORY

REPORT ON MERCURY TESTING

DRAFT REPORT REVISION HISTORY

Revision:	Date	Pages	Comments
D0a	01/04/11	All	Draft version of original document.

FINAL REPORT REVISION HISTORY

Revision:	Date	Pages	Comments
0	01/06/11	All	Final version of original document.

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PROJECT OVERVIEW

1-1

Wheelabrator North Broward, Inc. operates a refuse-to-energy facility, located in Pompano Beach, Florida. The facility's emission levels are regulated by the Florida Department of Environmental Protection (FDEP). Wheelabrator North Broward, Inc. contracted Clean Air Engineering (CleanAir) to perform a compliance test program at its municipal waste combustor (MWC) facility in Pompano Beach, Florida. Testing was conducted in accordance with 40 CFR 60 Subpart Cb and applicable sections of PSD-FL-112(B) and PA86-22. The sampling was conducted at the Unit 3 Fabric Filter (FF) Outlet on December 8, 2010.

The testing included the determination of the following constituents:

- moisture (H₂O)
- oxygen (O₂)
- carbon dioxide (CO₂)
- total flow (dscfm)
- mercury (Hg)

Coordinating and observing the field portion of the program were:

- B. Hooper - Wheelabrator
- C. Slimp - CleanAir
- K. Sullivan - CleanAir

Bill Hooper of Wheelabrator North Broward Inc. provided all the process (operating) data. This data is presented in its entirety in Appendix H.

All equipment utilized for testing was manufactured by Clean Air Engineering.

Table 1-1 outlines the schedule adhered to during the test program. Table 1-2 (on page 1-2) summarizes the results of the test program.

**Table 1-1:
Schedule of Activities**

Run Number	Location	Method	Analyte	Date	Start Time	End Time
1	Unit 3 FF Outlet	USEPA Method 29	Trace Metals	12/08/10	08:04	10:19
2	Unit 3 FF Outlet	USEPA Method 29	Trace Metals	12/08/10	10:45	12:53
3	Unit 3 FF Outlet	USEPA Method 29	Trace Metals	12/08/10	13:10	15:15

PROJECT OVERVIEW

1-2

**Table 1-2:
Summary of Test Results**

<u>Source</u> Constituent	Sampling Method	Average Emission	Permit Limit ¹
Unit 3 FF Outlet Mercury ($\mu\text{g}/\text{dscm}$ @7% O ₂)	EPA M29	5.3	50

¹ Limit obtained from the facility's Title V Permit No. 0570127-005-AV and Subpart Cb as of April 28, 2009.

The test conditions and results of analysis are presented in Table 2-1 (on page 2-1) and the quality control and quality assurance results are shown in Table 2-2 (on page 2-2).

End of Section 1 – Project Overview

RESULTS

2-1

**Table 2-1:
Unit 3 FF Outlet – Mercury**

Run No.	1	2	3	Average
Date (2010)	Dec 8	Dec 8	Dec 8	
Start Time (approx.)	08:04	10:45	13:10	
Stop Time (approx.)	10:19	12:53	15:15	
Process Conditions				
R _p Steam Production Rate (Klbs/hour)	180	180	180	180
P ₁ SDA Outlet Temperature (°F)	320	320	320	320
Gas Conditions				
O ₂ Oxygen (dry volume %)	10.7	10.7	10.1	10.5
CO ₂ Carbon dioxide (dry volume %)	8.3	8.2	8.9	8.5
T _s Sample temperature (°F)	306	307	309	307
B _w Actual water vapor in gas (% by volume)	19.8	19.0	19.4	19.4
Gas Flow Rate				
Q _a Volumetric flow rate, actual (acfm)	186,645	187,110	181,294	185,016
Q _{std} Volumetric flow rate, dry standard (dscfm)	100,911	102,101	98,113	100,375
Sampling Data				
V _{mstd} Volume metered, standard (dscf)	79.428	79.457	76.424	78.436
%I Isokinetic sampling (%)	100.7	99.5	99.6	99.9
Laboratory Data				
m _{n-1b} Fraction 1B (µg)	<0.1000	<0.1000	<0.1000	
m _{n-2b} Fraction 2B (µg)	7.9536	7.4497	10.7533	
m _{n-3a} Fraction 3A (µg)	<0.2000	0.3763	<0.2000	
m _{n-3b} Fraction 3B (µg)	<0.5000	<0.5000	<0.5000	
m _{n-3c} Fraction 3C (µg)	<0.4000	<0.4000	<0.4000	
m _n Total matter corrected for allowable blanks (µg)	7.9536	7.8260	10.7533	
Mercury Results - Total				
C _{sd} Concentration (lb/dscf)	2.21E-10	2.17E-10	3.10E-10	2.49E-10
C _{sd7} Concentration @7% O ₂ (lb/dscf)	3.02E-10	2.97E-10	4.01E-10	3.33E-10
C _{sd} Concentration (µg/dscm)	3.5	3.5	5.0	4.0
C _{sd7} Concentration @7% O ₂ (µg/dscm)	4.8	4.8	6.4	5.3
E _{lb/hr} Rate (lb/hr)	1.34E-03	1.33E-03	1.83E-03	1.50E-03
E _{Fd} Rate - Fd-based (lb/MMBtu)	4.34E-06	4.27E-06	5.76E-06	4.79E-06

RESULTS

2-2

**Table 2-2:
Quality Assurance and Quality Control**

		RPD RESULTS				
		FH	BH	A	B	C
		Front		Empty		
Run Number		Half	H₂O₂/HNO₄	Impinger	KMnO₄	HCl
		-----	-----	-----	-----	-----
U3 FF Outlet R1		NA	3.0%	NA	NA	NA
U3 FF Outlet R2		NA	4.5%	7.0%	NA	NA
U3 FF Outlet R3		NA	4.8%	NA	NA	NA
Field Blank		NA	NA	NA	NA	NA
Reagent Blank		NA	NA	NA	NA	NA
Sample Spike and Recovery						
U3 FF Outlet R3	#1	115%	106%	117%	112%	105%
	#2	113%	110%	109%	113%	94%
Blanks						
Field Blank	#1	< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
	#2	< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
Reagent Blank	#1	< 0.1	< 0.2	< 0.2	< 0.5	< 0.4
	#2	< 0.1	< 0.2	< 0.2	< 0.5	< 0.4
Meter Post Cal		-0.4%				

End of Section 2 – Results

DESCRIPTION OF INSTALLATION

PROCESS DESCRIPTION

The North Broward Resource Recovery facility operates three (3) 750 tons per day municipal refuse-fired, water-wall boiler trains. The trains were manufactured by Babcock & Wilcox to produce electricity for sale to a local utility company. Each boiler is equipped with a spray dryer absorber (SDA) for acid gas removal, followed by an FF baghouse for the control of particulate emissions. Wheelabrator Air Pollution Control, Inc. supplies the control equipment. Each FF baghouse is followed by an induced draft fan that directs the flue gas to a dedicated flue in a common stack.

Figure 3-1 shows a general schematic for the facility. The testing occurred at the Unit 3 FF outlet, as shown in Figure 3-2 (on page 3-2).

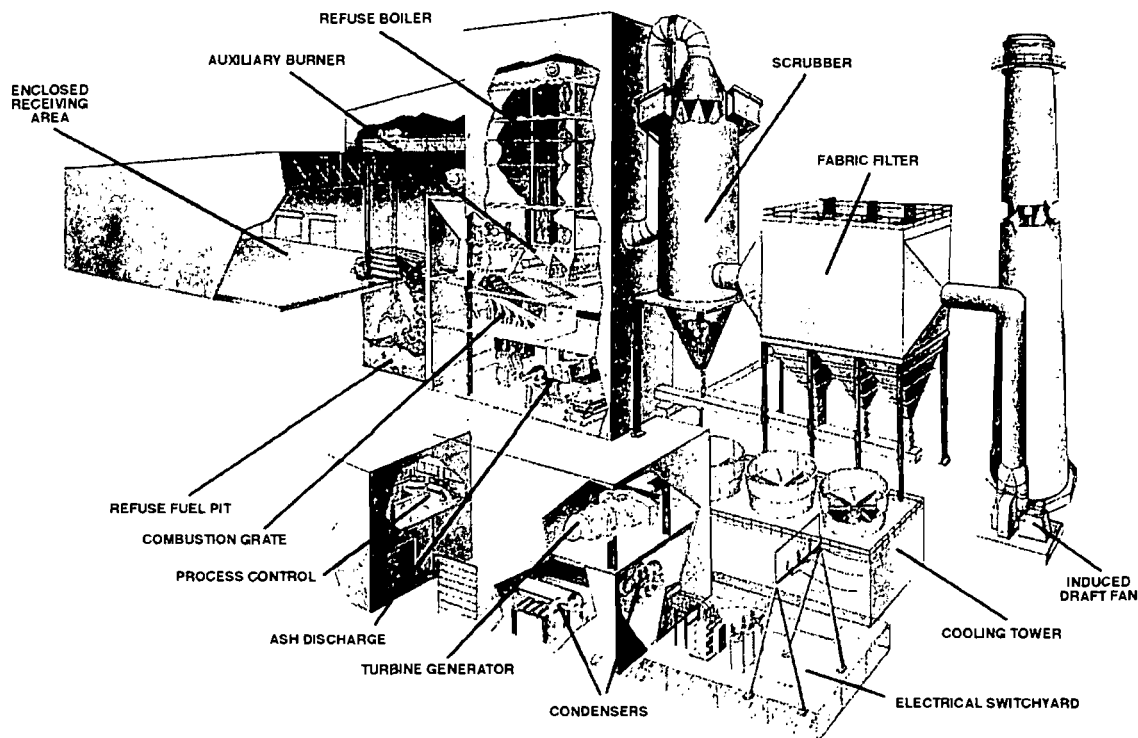


Figure 3-1: General Process Schematic

DESCRIPTION OF INSTALLATION
PROCESS DESCRIPTION (CONTINUED)

3-2

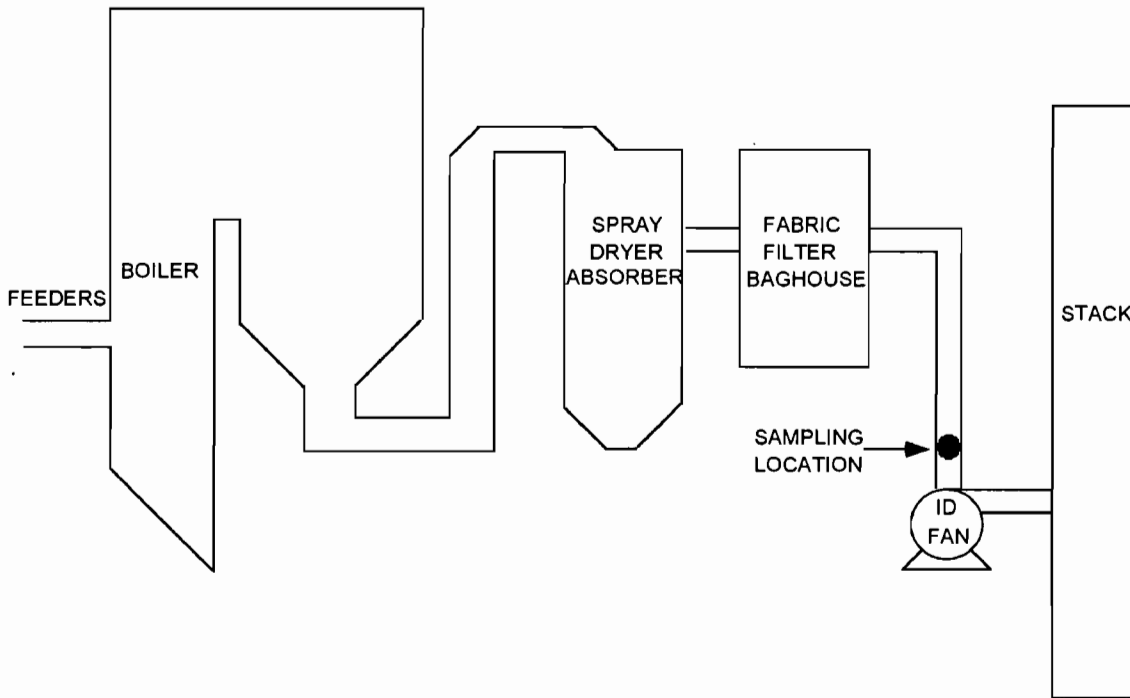


Figure 3-2: Process Schematic

DESCRIPTION OF INSTALLATION

3-3

DESCRIPTION OF SAMPLING LOCATION

The sampling point location was determined according to EPA Method 1.

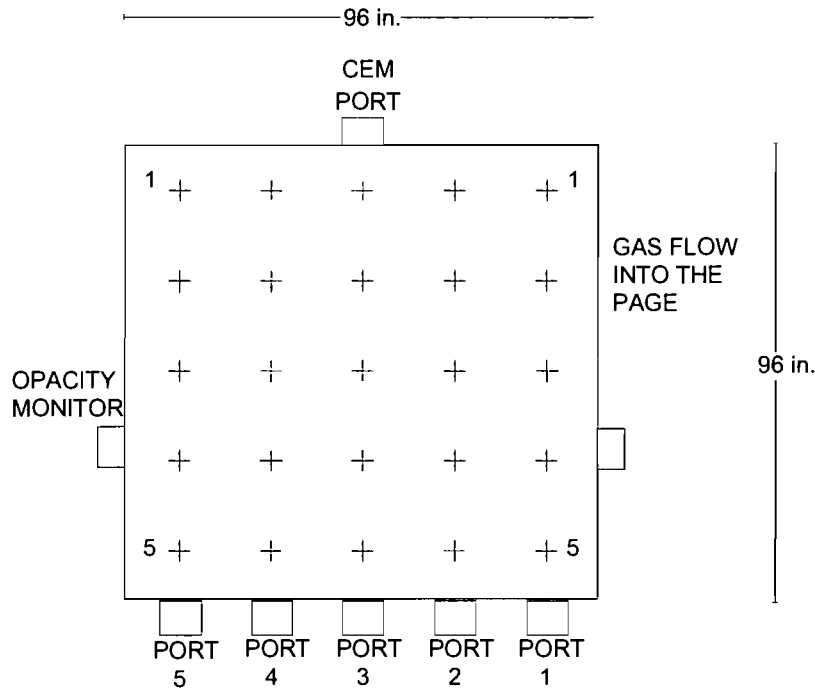
Table 3-1 outlines the sampling point configurations. Figure 3-3 (on page 3-4) illustrates the sampling points and orientation of sampling ports for the source tested in the program.

**Table 3-1:
Sampling Points**

Location	Constituent	Method	Run No.	Ports	Points per Port	Minutes per Point	Total Minutes	Figure
Unit 3 FF Outlet	Mercury	29	1-3	5	5	5	125	3-3

DESCRIPTION OF INSTALLATION
DESCRIPTION OF SAMPLING LOCATION (CONTINUED)

3-4



<u>Sampling Point</u>	<u>Port to Point Distance (in.)</u>
1	86.4
2	67.2
3	48.0
4	28.8
5	9.6

Equivalent Duct diameters upstream from flow disturbance (A): 0.5 Limit: 0.5
Equivalent Duct diameters downstream from flow disturbance (B): 2.0 Limit: 2.0

Figure 3-3: Unit 3 FF Outlet Sampling Point Determination (EPA Method 1)

End of Section 3 – Description of Installation

METHODOLOGY

4-1

Clean Air Engineering followed procedures as detailed in U.S. Environmental Protection Agency (EPA) Methods 1, 2, 3, 3B, 4 and 29. The following table summarizes the methods and their respective sources.

**Table 4-1:
Summary of Sampling Procedures**

Title 40 CFR Part 60 Appendix A

Method 1	"Sample and Velocity Traverses for Stationary Sources"
Method 2	"Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)"
Method 3	"Gas Analysis for the Determination of Dry Molecular Weight"
Method 3B	"Gas Analysis for the Determination of Emission Rate Correction Factor or Excess Air"
Method 4	"Determination of Moisture Content in Stack Gases"
Method 29	"Determination of Metals Emissions from Stationary Sources"

These methods appear in detail in Title 40 of the Code of Federal Regulations (CFR) and on the World Wide Web at <http://www.cleanair.com>.

Diagrams of the sampling apparatus and major specifications of the sampling, recovery and analytical procedures are summarized for each method in Appendix A.

CleanAir followed specific quality assurance and quality control (QA/QC) procedures as outlined in the individual methods and in EPA "Quality Assurance Handbook for Air Pollution Measurement Systems: Volume III Stationary Source-Specific Methods", EPA/600/R-94/038C. Additional QA/QC methods, as prescribed in CleanAir's internal Quality Manual, were also followed. Results of all QA/QC activities performed by CleanAir are summarized in Appendix D.

End of Section 4 –Methodology

WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-7

APPENDIX

5-1

TEST METHOD SPECIFICATIONS	A
SAMPLE CALCULATIONS	B
PARAMETERS	C
QA/QC DATA	D
FIELD DATA	E
FIELD DATA PRINTOUTS	F
LABORATORY DATA	G
PLANT DATA	H

WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-7

TEST METHOD SPECIFICATIONS

A

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Specification Sheet for

EPA Method 29

Source Location Name(s) Unit 3 FF Outlet
 Pollutant(s) to be Determined Mercury
 Other Parameters to be Determined from Train Gas Density, Moisture, Flow Rate

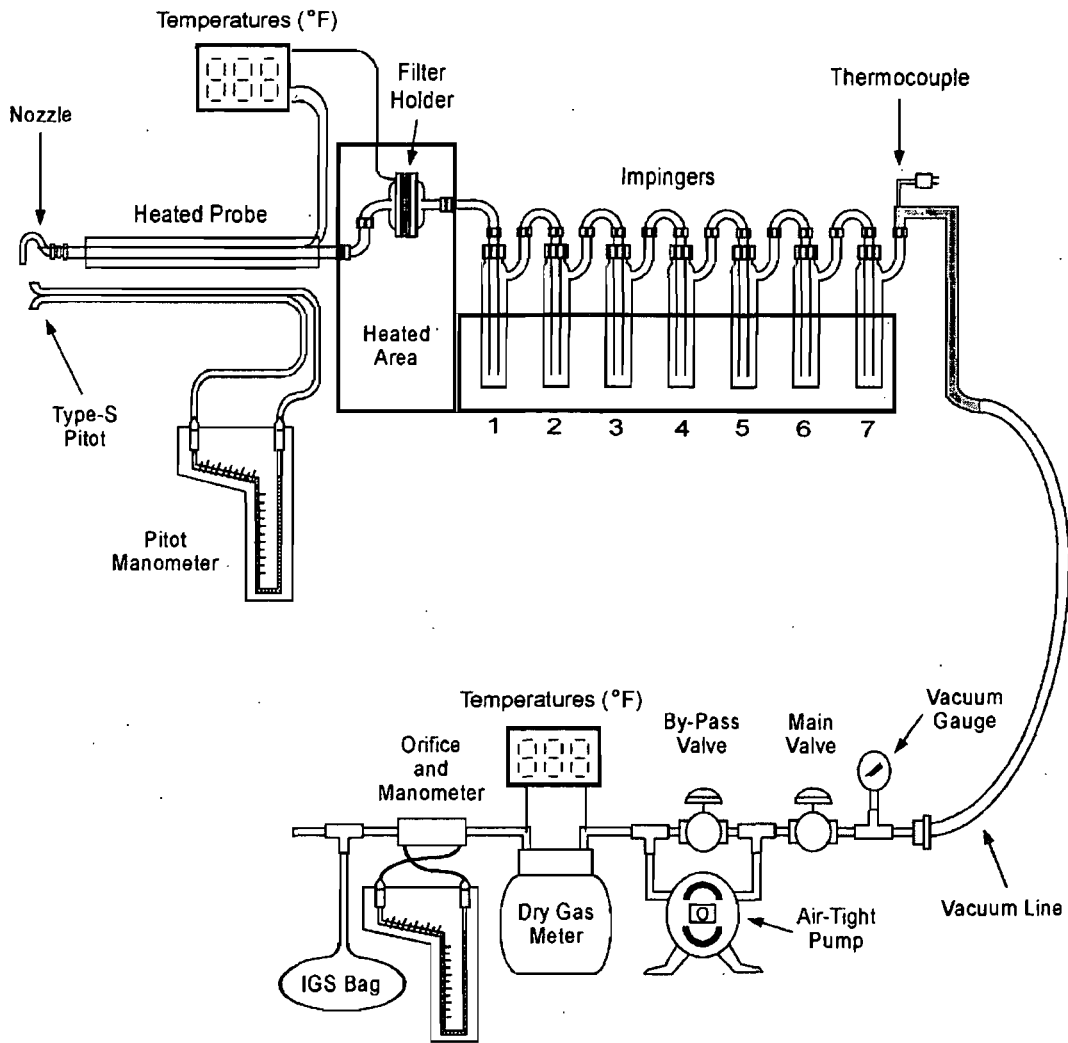
	Standard Method Specification	Actual Specification Used
Pollutant Sampling Information		
Duration of Run	N/A	125 minutes
No. of Sample Traverse Points	N/A	25
Sample Time per Point	N/A	5 minutes
Sampling Rate	Isokinetic (90-110%)	Isokinetic (90-110%)
Sampling Probe		
Nozzle Material	Borosilicate or Quartz Glass	Borosilicate Glass
Nozzle Design	Button-Hook or Elbow	Button-Hook
Probe Liner Material	Borosilicate or Quartz Glass	Borosilicate Glass
Effective Probe Length	N/A	8 feet
Probe Temperature Set-Point	248°F±25°F	248°F±25°F
Velocity Measuring Equipment		
Pitot Tube Design	Type S	Type S
Pitot Tube Coefficient	N/A	0.82
Pitot Tube Calibration by	Geometric or Wind Tunnel	Wind-Tunnel
Pitot Tube Attachment	Attached to Probe	Attached to Probe
Metering System Console		
Meter Type	Dry Gas Meter	Dry Gas Meter
Meter Accuracy	±2%	±1%
Meter Resolution	N/A	0.01 cubic feet
Meter Size	N/A	0.1 dcf/revolution
Meter Calibrated Against	Wet Test Meter or Standard DGM	Wet Test Meter
Pump Type	N/A	Rotary Vane
Temperature Measurements	N/A	Type K Thermocouple/Pyrometer
Temperature Resolution	5.4°F	1.0°F
ΔP Differential Pressure Gauge	Inclined Manometer or Equivalent	Inclined Manometer
ΔH Differential Pressure Gauge	Inclined Manometer or Equivalent	Inclined Manometer
Barometer	Mercury or Aneroid	Digital Barometer calibrated w/Mercury Aneroid
Filter Description		
Filter Location	After Probe	Exit of Probe
Filter Holder Material	Borosilicate Glass	Borosilicate Glass
Filter Support Material	Teflon (or other non-metallic)	Teflon
Cyclone Material	N/A	None
Filter Heater Set-Point	248°F±25°F	248°F±25°F
Filter Material	Quartz or Glass Fiber	Quartz Fiber
Other Components		
Description	N/A	N/A
Location	N/A	N/A
Operating Temperature	N/A	N/A

Specification Sheet for

EPA Method 29

	<u>Standard Method Specification</u>	<u>Actual Specification Used</u>
Impinger Train Description		
Type of Glassware Connections	Ground Glass or Equivalent	Screw Joint with Silicone Gasket
Connection to Probe or Filter by	Direct Glass Connection	Direct Glass Connection
Number of Impingers	7	7
Impinger Stem Types		
Impinger 1	Modified Greenburg-Smith	Modified Greenburg-Smith
Impinger 2	Modified Greenburg-Smith	Modified Greenburg-Smith
Impinger 3	Greenburg-Smith	Greenburg-Smith
Impinger 4	Modified Greenburg-Smith	Modified Greenburg-Smith
Impinger 5	Modified Greenburg-Smith	Modified Greenburg-Smith
Impinger 6	Modified Greenburg-Smith	Modified Greenburg-Smith
Impinger 7	Modified Greenburg-Smith	Modified Greenburg-Smith
Impinger 8		
Gas Density Determination		
Sample Collection	Multi-point integrated	Multi-Point Integrated
Sample Collection Medium	Flexible Gas Bag	Vinyl Bag
Sample Analysis	Orsat or Fyrite Analyzer	Orsat
Sample Recovery Information		
Probe Brush Material	Non-metallic swab or bristle	Teflon Mat
Probe Rinse Reagent	0.1N Nitric Acid	0.1 N Nitric Acid
Probe Rinse Wash Bottle Material	Glass or Teflon	Teflon
Probe Rinse Storage Container	Polyethylene or glass	Polyethylene
Filter Recovered?	Yes	Yes
Filter Storage Container	Petri Dish - Glass or Polystyrene	Polyethylene
Impinger Contents Recovered?	Yes	Yes
Impinger Rinse Reagent	See Method 29 Recovery Flow Chart	See Recovery Flow Chart
Impinger Wash Bottle	Glass or Teflon	Teflon
Impinger Storage Container	See Recovery Flow Chart	See Recovery Flow Chart
Analytical Information		
Method 4 H ₂ O Determination by	Volumetric or Gravimetric	Gravimetric and Volumetric
Filter Preparation Conditions	See Method 29 Analytical Flow Chart	For Metals Analysis
Front-Half Rinse Preparation	See Method 29 Analytical Flow Chart	See Analytical Flow Chart
Back-Half Analysis	See Method 29 Analytical Flow Chart	See Analytical Flow Chart
Additional Analysis	None	None

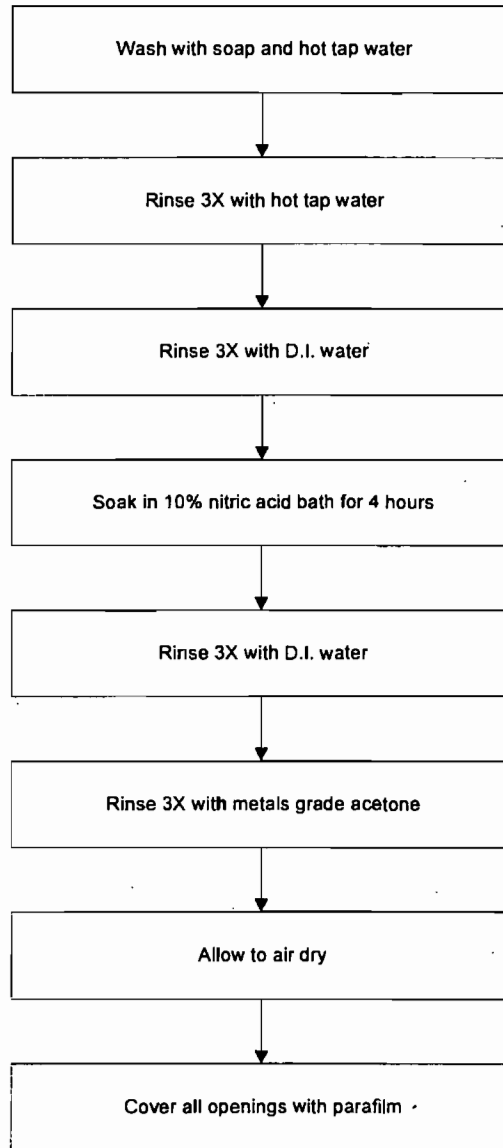
EPA Method 29 Sampling Train Configuration



Impinger Contents

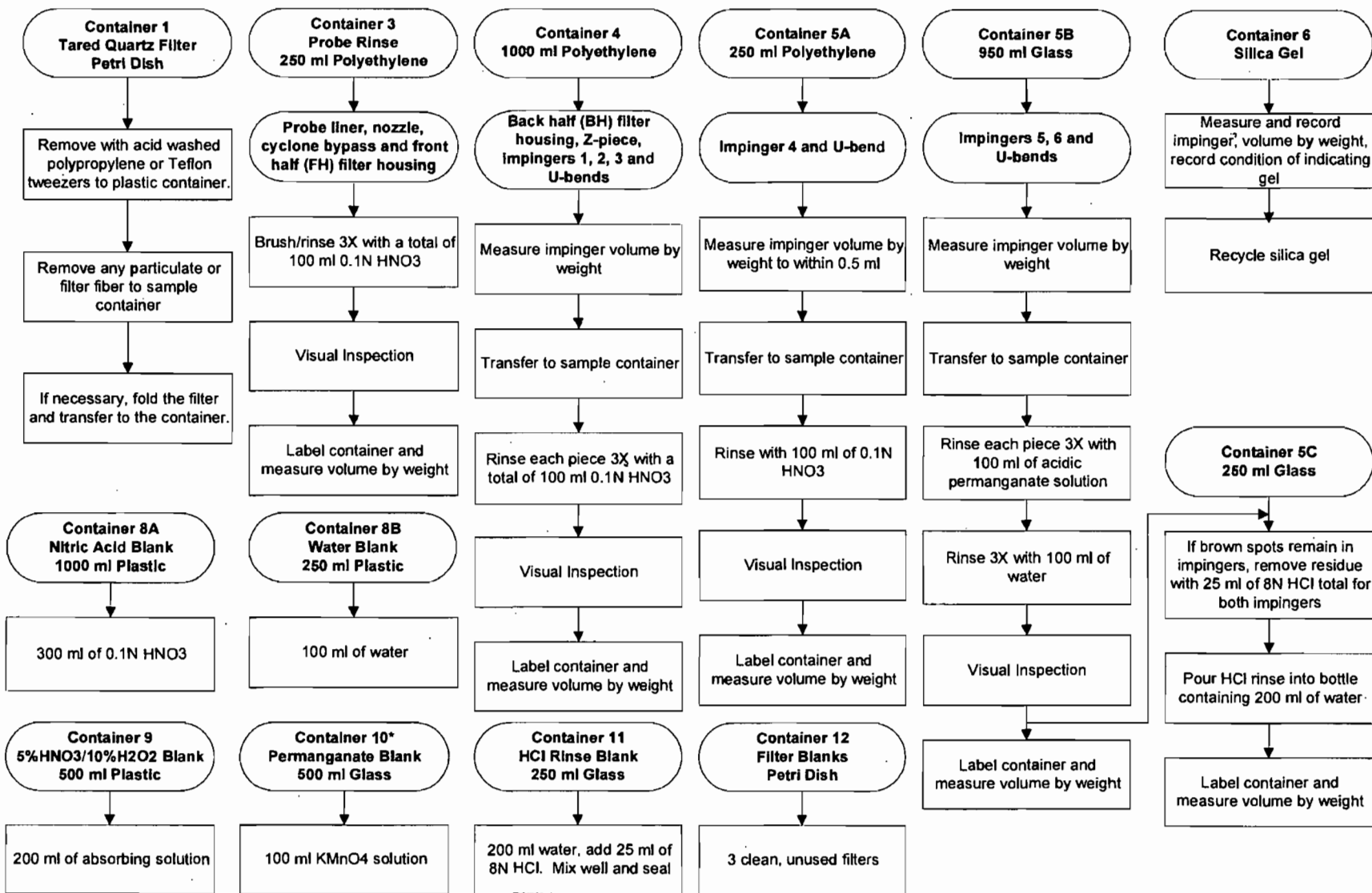
Impinger 1	Empty
Impinger 2	100 ml 5% HNO ₃ /10% H ₂ O ₂
Impinger 3	100 ml 5% HNO ₃ /10% H ₂ O ₂
Impinger 4	Empty
Impinger 5	100 ml 4% KMnO ₄ /10% H ₂ SO ₄
Impinger 6	100 ml 4% KMnO ₄ /10% H ₂ SO ₄
Impinger 7	Silica Gel

EPA Method 29 Glassware Preparation Procedures

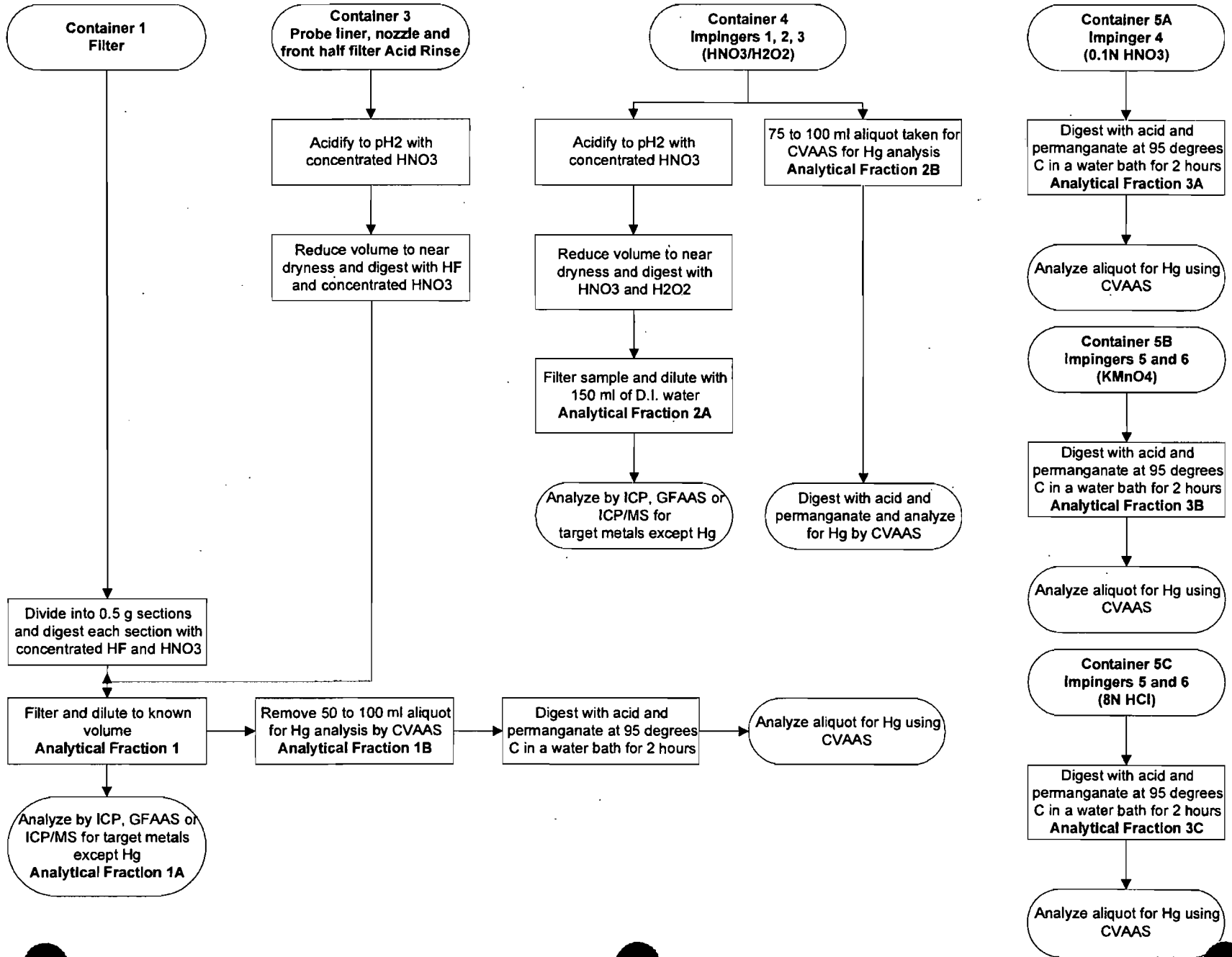


EPA Method 29
Sample Recovery Flowchart
 (Includes Mercury)

- Tare all sample containers before sample collection
- Mark all liquid levels and final weights on the outside of each sample container
- Seal all sample containers with Teflon tape
- If recycling, bake silica gel for two hours at 350 degrees F (175 degrees C)
- Collect one complete blank set per field test



EPA Method 29
Analytical Flowchart
 (includes Mercury)



WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-7

SAMPLE CALCULATIONS

B

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**USEPA Method 29 (Trace Metals)
 Sampling, Velocity and Moisture Sample Calculations**

Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

122110 120811

1. Volume of water collected (wscf)

$$V_{wstd} = (0.04706)(V_{lc})$$

Where:

V_{lc}	= total volume of liquid collected in impingers and silica gel (ml)	=	416.5	ml
0.04706	= ideal gas conversion factor (ft ³ water vapor/ml or gm)	=	0.04706	ft ³ /ml
V_{wstd}	= volume of water vapor collected at standard conditions (ft ³)	=	19.60	ft ³

2. Volume of gas metered, standard conditions (dscf)

$$V_{mstd} = \frac{(17.64)(V_m) \left(P_{bar} + \frac{\Delta H}{13.6} \right) (Y_d)}{(460 + T_m)}$$

Where:

P_{bar}	= barometric pressure (in. Hg)	=	30.04	in. Hg
T_m	= average dry gas meter temperature (°F)	=	51.12	°F
V_m	= volume of gas sample through the dry gas meter at meter conditions (dcf)	=	76.69	dcf
Y_d	= gas meter correction factor (dimensionless)	=	0.9960	
ΔH	= average pressure drop across meter box orifice (in. H ₂ O)	=	1.22	in. H ₂ O
17.64	= standard temperature to pressure ratio (°R/in. Hg)	=	17.64	°R/in. Hg
13.6	= conversion factor (in. H ₂ O/in. Hg)	=	13.6	in. H ₂ O/in. Hg
460	= °F to °R conversion constant	=	460	
V_{mstd}	= volume of gas sampled through the dry gas meter at standard conditions (dscf)	=	79.428	dscf

3. Sample gas pressure (in. Hg)

$$P_s = P_{bar} + \left(\frac{P_g}{13.6} \right)$$

Where:

P_{bar}	= barometric pressure (in. Hg)	=	30.04	in. Hg
P_g	= sample gas static pressure (in. H ₂ O)	=	-10.70	in. H ₂ O
13.6	= conversion factor (in. H ₂ O/in. Hg)	=	13.6	in. H ₂ O/in. Hg
P_s	= absolute sample gas pressure (in. Hg)	=	29.25	in. Hg

4. Actual water vapor pressure at sample gas temperature less than 212°F (in. Hg)

$$P_v = \frac{e^{\left(\frac{18.3036 - \frac{3816.44}{\frac{5}{9}(T_s - 32) + 273.15 - 46.13}}{25.4} \right)}}{25.4}$$

Where:

T_s	= average sample gas temperature (°F)	=	305.84	°F
18.3036	= Antoine coefficient	=	18.3036	°K
3816.44	= Antoine coefficient	=	3816.44	°K
273.15	= temperature conversion factor	=	273.15	°K
46.13	= Antoine coefficient	=	46.13	°K
25.4	= conversion factor	=	25.4	mm Hg/in. Hg
5/9	= Fahrenheit to Celsius conversion factor	=	5/9	°C/°F
32	= temperature conversion (°F)	=	32	°F
P_v	= vapor pressure, actual (in. Hg)	=	29.25	in. Hg

5. Water vapor pressure at gas temperature greater than 212°F (in. Hg)

$$P_v = P_s$$

Where:

P_s	= absolute sample gas pressure (in. Hg)	=	29.25	in. Hg
P_v	= water vapor pressure, actual (in. Hg)	=	29.25	in. Hg

6. Moisture measured in sample (% by volume)

$$B_{wo} = \frac{V_{wstd}}{(V_{mstd} + V_{wstd})}$$

Where:

V_{mstd}	= volume of gas sampled through the dry gas meter at standard conditions (dscf)	=	79.428	dscf
V_{wstd}	= volume of water collected at standard conditions (scf)	=	19.60	scf
B_{wo}	= proportion of water measured in the gas stream by volume	=	0.1979	
		=	19.79	%

7. Saturated moisture content (% by volume)

$$B_{ws} = \frac{P_v}{P_s}$$

Where:

P_s	= absolute sample gas pressure (in. Hg)	=	29.25	in. Hg
P_v	= water vapor pressure, actual (in. Hg)	=	29.25	in. Hg
B_{ws}	= proportion of water vapor in the gas stream by volume at saturated conditions	=	1.0000	
		=	100.00	%

8. Actual water vapor in gas (% by volume)

$$B_w = \text{MINIMUM} [B_{wo}, B_{ws}]$$

Where:

B_{ws}	= proportion of water vapor in the gas stream by volume at saturated conditions	=	1.0000	
B_{wo}	= proportion of water measured in the gas stream by volume	=	0.1979	
B_w	= actual water vapor in gas	=	0.1979	
		=	19.79	%

9. Nitrogen (plus carbon monoxide) in gas stream (% by volume, dry)

$$N_2 + CO = 100 - CO_2 - O_2$$

Where:

CO_2	= proportion of carbon dioxide in the gas stream by volume (%)	=	8.3	%
O_2	= proportion of oxygen in the gas stream by volume (%)	=	10.7	%
100	= conversion factor (%)	=	100	%
N_2+CO	= proportion of nitrogen and CO in the gas stream by volume (%)	=	81.00	%

10. Molecular weight of dry gas stream (lb/lb-mole)

$$M_d = \left(M_{CO_2} \right) \frac{(CO_2)}{(100)} + \left(M_{O_2} \right) \frac{(O_2)}{(100)} + \left(M_{N_2+CO} \right) \frac{(N_2+CO)}{(100)}$$

Where:

M_{CO_2}	= molecular weight of carbon dioxide (lb/lb-mole)	=	44.00	lb/lb-mole
M_{O_2}	= molecular weight of oxygen (lb/lb-mole)	=	32.00	lb/lb-mole
M_{N_2+CO}	= molecular weight of nitrogen and carbon monoxide (lb/lb-mole)	=	28.00	lb/lb-mole
CO_2	= proportion of carbon dioxide in the gas stream by volume (%)	=	8.3	%
O_2	= proportion of oxygen in the gas stream by volume (%)	=	10.7	%
N_2+CO	= proportion of nitrogen and CO in the gas stream by volume (%)	=	81.0	%
100	= conversion factor (%)	=	100	%
M_d	= dry molecular weight of sample gas (lb/lb-mole)	=	29.75	lb/lb-mole

11. Molecular weight of sample gas (lb/lb-mole)

$$M_s = (M_d)(1 - B_w) + (M_{H_2O})(B_w)$$

Where:

B_w	= proportion of water vapor in the gas stream by volume	=	0.1979	
M_d	= dry molecular weight of sample gas (lb/lb-mole)	=	29.75	lb/lb-mole
M_{H_2O}	= molecular weight of water (lb/lb-mole)	=	18.00	lb/lb-mole
M_s	= molecular weight of sample gas, wet basis (lb/lb-mole)	=	27.43	lb/lb-mole

12. Velocity of sample gas (ft/sec)

$$V_s = (K_p)(C_p)\sqrt{\Delta P} \left(\sqrt{\frac{T_s + 460}{(M_s)(P_s)}} \right)$$

Where:

K_p	= velocity pressure constant	=	85.49	
C_p	= pitot tube coefficient	=	0.82	
M_s	= wet molecular weight of sample gas, wet basis (lb/lb-mole)	=	27.43	lb/lb-mole
P_s	= absolute sample gas pressure (in. Hg)	=	29.25	in. Hg
T_s	= average sample gas temperature (°F)	=	305.84	°F
$\sqrt{\Delta P}$	= average square roots of velocity heads of sample gas (in. H ₂ O)	=	0.710	$\sqrt{\text{in. H}_2\text{O}}$
460	= °F to °R conversion constant	=	460	
V_s	= sample gas velocity (ft/sec)	=	48.61	ft/sec

13. Volumetric flow rate of sample gas at actual gas conditions (acfm)

$$Q_a = (60)(A_s)(V_s)$$

Where:

A_s	= cross sectional area of sampling location (ft ²)	=	64.00	ft ²
V_s	= sample gas velocity (ft/sec)	=	48.61	ft/sec
60	conversion factor (sec/min)	=	60	sec/min
Q_a	= volumetric flow rate at actual conditions (acfm)	=	186,645	acfm

14. Total flow of sample gas (scfm)

$$Q_s = (Q_a) \left(\frac{P_s}{29.92} \right) \left(\frac{68 + 460}{T_s + 460} \right)$$

Where:

Q_a	= volumetric flow rate at actual conditions (acfm)	=	186,645	acfm
P_s	= absolute sample gas pressure (in. Hg)	=	29.25	in. Hg
29.92	= standard pressure (in. Hg)	=	29.92	in. Hg
T_s	= average sample gas temperature (°F)	=	305.8	°F
68	= standard temperature (°F)	=	68	°F
460	= °F to °R conversion constant	=	460	
Q_s	= volumetric flow rate at standard conditions, wet basis (scfm)	=	125,812	scfm

15. Dry flow of sample gas (dscfm)

$$Q_{std} = (Q_s)(1 - B_w)$$

Where:

B_w	= proportion of water vapor in the gas stream by volume	=	0.1979	
Q_s	= volumetric flow rate at standard conditions, wet basis (scfm)	=	125,812	scfm
Q_{std}	= volumetric flow rate at standard conditions, dry basis (dscfm)	=	100,911	dscfm

16. Dry flow of sample gas corrected to 7%O₂ (dscfm)

$$Q_{std\ 7} = (Q_{std}) \left(\frac{20.9 - O_2}{20.9 - 7} \right)$$

Where:

Q _{std}	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 100,911	dscfm
O ₂	= proportion of oxygen in the gas stream by volume (%)	= 10.7	%
20.9	= oxygen content of ambient air (%)	= 20.9	%
7	= oxygen content of corrected gas (%)	= 7.0	%
Q _{std7}	= volumetric flow rate at STP and 7%O ₂ , dry basis (dscfm)	= 73,808	dscfm

17. Hourly time basis conversion of volumetric flow rate (Q_{std} example)

$$Q_{std\ -\ hr} = (Q_{std\ -\ min}) (60)$$

Where

Q _{std-min}	= volumetric flow rate, english units (ft ³ /min)	= 100,911	dscfm
60	= conversion factor (min/hr)	= 60	min/hr
Q _{std-hr}	= volumetric flow rate, hourly basis (dscf/hr)	= 6,054,636	dscf/hr

18. Metric Conversion of Gas Volumes (Q_{std} example)

$$Q_{std\ -\ metric} = (Q_{std\ -\ english}) \left(\frac{60}{35.31} \right)$$

Where:

Q _{std-english}	= volumetric flow rate, english units (ft ³ /min)	= 100,911	dscfm
35.31	= conversion factor (ft ³ /m ³)	= 35.31	ft ³ /m ³
60	= conversion factor (min/hr)	= 60	min/hr
Q _{std-metric}	= volumetric flow rate, metric units (m ³ /hr)	= 171,471	dry std m ³ /hr

19. Standard to Normal Conversion of Gas Volumes (Q_{std} example)

$$Q_{Normal} = (Q_{std\ -\ metric}) \left(\frac{32 + 460}{68 + 460} \right)$$

Where:

Q _{std-metric}	= volumetric flow rate, metric units (dry std m ³ /hr)	= 171,471	dry std m ³ /hr
32	= normal temperature (°F)	= 32	°F
68	= standard temperature (°F)	= 68	°F
460	= standard temperature in Rankine (68°F)	= 460	
Q _{Normal}	= volumetric flow rate, metric units (dry Nm ³ /hr)	= 159,780	dry Nm ³ /hr

20. Percent isokinetic (%)

$$I = \frac{(0.09450)(T_s + 460)(V_{mstd})}{(P_s)(V_s)\left(\frac{D_n^2(r)}{144(4)}\right)(\Theta)(1 - B_w)}$$

Where:

D_n	= diameter of nozzle (in)	=	0.271	in.
B_w	= proportion of water vapor in the gas stream by volume	=	0.1979	
P_s	= absolute sample gas pressure (in. Hg)	=	29.25	in. Hg
T_s	= average sample gas temperature (°F)	=	305.8	°F
V_{mstd}	= volume of gas sample through the dry gas meter at standard conditions (dscf)	=	79.428	dscf
V_s	= sample gas velocity (ft/sec)	=	48.61	ft/sec
θ	= total sampling time (min)	=	125	min
0.0945	= conversion constant	=	0.0945	
460	= °F to °R conversion constant	=	460	
I	= percent of isokinetic sampling (%)	=	100.67	%

21. Alternative Method 5 Post-Test Meter Calibration Factor

$$Y_{qa} = \frac{\Theta}{V_m} \sqrt{\frac{(0.0319)(T_m + 460)(28.96)}{(\Delta H_{@})(P_{bar} + \frac{\Delta H}{13.6})(M_d)}} (\sqrt{\Delta H})_{avg}$$

Where:

θ	= total sampling time (min)	=	125	min
V_m	= volume of gas sample through the dry gas meter at meter conditions (dcf)	=	76.69	dcf
T_m	= average dry gas meter temperature (°F)	=	51.12	°F
$\Delta H_{@}$	= dry gas meter orifice coefficient	=	1.7601	
P_{bar}	= barometric pressure (in. Hg)	=	30.04	in. Hg
ΔH	= average pressure drop across meter box orifice (in. H ₂ O)	=	1.223	in. H ₂ O
M_d	= dry molecular weight of sample gas (lb/lb-mole)	=	29.75	lb/lb-mole
$\sqrt{\Delta H}_{avg}$	= average of square root of pressure drop across meter orifice	=	1.102	$\sqrt{\text{in. H}_2\text{O}}$
0.0319	= conversion constant	=	0.0319	
28.96	= molecular weight of ambient air (lb/lb-mole)	=	28.96	lb/lb-mole
13.6	= conversion factor (in. H ₂ O/in. Hg)	=	13.6	in. H ₂ O/in. Hg
460	= °F to °R conversion constant	=	460	
Y_{qa}	= alternative Method 5 post-test meter calibration factor	=	0.9826	

LOGIC FOR TREATING DETECTION LIMITS (mercury only)

1. Logic for Determining Total Blank ($m_{Total-B}$) from 5 Fractions

	CASE 1 All 5 fractions are D.	CASE 2 1 to 4 fractions are ND	CASE 3 All 5 fractions are ND
Rule			
$ND = 0$	$m_{Total-B} = \text{Sum D, 1-5}$	$m_{Total-B} = \text{Sum D}$	$m_{Total-B} = < \text{Sum ND}$
$ND = 1x$	$m_{Total-B} = \text{Sum D, 1-5}$	$m_{Total-B} = \text{Sum D}$	$m_{Total-B} = < \text{Sum ND}$
$ND = 0.5x$	$m_{Total-B} = \text{Sum D, 1-5}$	$m_{Total-B} = \text{Sum D}$	$m_{Total-B} = < 0.5 \text{ Sum ND}$

2. Logic for Determining Total Sample ($m_{Total-S}$) from 5 Fractions

	CASE 1 All 5 fractions are D.	CASE 2 1 to 4 fractions are ND	CASE 3 All 5 fractions are ND
Rule			
$ND = 0$	$m_{Total-S} = \text{Sum D, 1-5}$	$m_{Total-S} = \text{Sum D}$	$m_{Total-S} = < \text{Sum ND}$
$ND = 1x$	$m_{Total-S} = \text{Sum D, 1-5}$	$m_{Total-S} = < [\text{Sum D} + \text{Sum ND}]$	$m_{Total-S} = < \text{Sum ND}$
$ND = 0.5x$	$m_{Total-S} = \text{Sum D, 1-5}$	$m_{Total-S} = < [\text{Sum D} + 0.5 \text{ Sum ND}]$	$m_{Total-S} = < 0.5 \text{ Sum ND}$

3. Logic for Determining Maximum Allowable Blank Correction ($m_{T-B-allow}$)

	CASE 1 All 5 fractions are D.	CASE 2 1 to 4 sample fractions are ND	CASE 3 All 5 fractions are ND	CASE 4 Any type of fractions
	$m_{Total-B} = D$	$m_{Total-B} = D$	$m_{Total-B} = D$	$m_{Total-B} = ND$
Rule				
$ND = 0$	$m_{T-B-allow} = \text{M29 Rule}$	$m_{T-B-allow} = \text{M29 Rule}$	$m_{T-B-allow} = 0$	$m_{T-B-allow} = 0$
$ND = 1x$	$m_{T-B-allow} = \text{M29 Rule}$	$m_{T-B-allow} = \text{M29 Rule}$	$m_{T-B-allow} = 0$	$m_{T-B-allow} = 0$
$ND = 0.5x$	$m_{T-B-allow} = \text{M29 Rule}$	$m_{T-B-allow} = \text{M29 Rule}$	$m_{T-B-allow} = 0$	$m_{T-B-allow} = 0$

* M29 rule using only detected sample quantities for logical comparisons.

4. Logic for Determining Blank-Corrected Sample Amount (m_n)

	CASE 1 All 5 fractions are D.	CASE 2 1 to 4 sample fractions are ND	CASE 3 All 5 fractions are ND	CASE 4 Any type of fractions
	$m_{Total-S} - m_{T-B-allow} \geq \text{MIN(MDL)}$	$m_{Total-S} - m_{T-B-allow} \geq \text{MIN(MDL)}$	$m_{Total-S}$ and $m_{T-B-allow}$ anything	$m_{Total-S} - m_{T-B-allow} < \text{MIN(MDL)}$
Rule				
$ND = 0$	$m_n = m_{Total-S} - m_{T-B-allow}$	$m_n = m_{Total-S} - m_{T-B-allow}$	$m_n = < m_{Total-S}$	$m_n = < \text{MIN(MDL)}$
$ND = 1x$	$m_n = m_{Total-S} - m_{T-B-allow}$	$m_n = < [m_{Total-S} - m_{T-B-allow}]$	$m_n = < m_{Total-S}$	$m_n = < \text{MIN(MDL)}$
$ND = 0.5x$	$m_n = m_{Total-S} - m_{T-B-allow}$	$m_n = < [m_{Total-S} - m_{T-B-allow}]$	$m_n = < m_{Total-S}$	$m_n = < \text{MIN(MDL)}$

Definitions and Notes

The term "Rule" refers to the rule being implemented for handling non-detectable quantities in summations.

MDL = minimum detection limit.

D = Detectable quantity reported as D.

ND = Non-Detectable quantity reported at a value of ND.

MIN(MDL) = lowest quantity of all detection limits for 5 fractions.

**USEPA Method 29
 Mercury Analyte Calculations**

Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

Note: Please see the preceding page concerning treatment of minimum detection limits and mathematical operations on values that are below minimum detection limits.

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 N

1. Total blank amount (µg)

$$m_{total-B} = \sum_{i=1}^n m_{i-B}$$

Where:

m_{1b-B}	= mercury amount in blank for Fraction 1b	= <0.1000	µg
m_{2b-B}	= mercury amount in blank for Fraction 2b	= <0.2000	µg
m_{3a-B}	= mercury amount in blank for Fraction 3a	= <0.2000	µg
m_{3b-B}	= mercury amount in blank for Fraction 3b	= <0.5000	µg
m_{3c-B}	= mercury amount in blank for Fraction 3c	= <0.4000	µg
$m_{total-B}$	= total amount of mercury in blank	= <1.4000	µg

2. Total sample amount (µg)

$$m_{total-S} = \sum_{i=1}^n m_{i-S}$$

Where:

m_{1b-S}	= mercury amount in sample for Fraction 1b	= <0.1000	µg
m_{2b-S}	= mercury amount in sample for Fraction 2b	= 7.9536	µg
m_{3a-S}	= mercury amount in sample for Fraction 3a	= <0.2000	µg
m_{3b-S}	= mercury amount in sample for Fraction 3b	= <0.5000	µg
m_{3c-S}	= mercury amount in sample for Fraction 3c	= <0.4000	µg
$m_{total-S}$	= total amount of mercury in sample	= 7.9536	µg

3. Allowable blank correction (µg)

$$m_{T-B-allow} = m_{total-B} \text{ if } m_{total-B} \leq 0.6$$

$$m_{T-B-allow} = \text{MAX} [0.6, \text{MIN} (m_{total-B}, 0.05 \times m_{total-S})] \text{ if } m_{total-B} > 0.6$$

Where:

$m_{total-B}$	= total amount of mercury in blank	= <1.4000	µg
$m_{total-S}$	= total amount of mercury in sample	= 7.9536	µg
$0.05 \times m_{total-S}$	= 5% of $m_{total-S}$	= 0.3977	µg
MAX	= arithmetic operator that returns the maximum of two values		
MIN	= arithmetic operator that returns the minimum of two values		
$m_{T-B-allow}$	= total allowable blank correction	= 0.0000	µg

NOTE: In this case, the second criteria applies.

4. Sample corrected for allowable blank - Total (µg)

$$m_n = m_{total-S} - m_{T-B-allow}$$

Where:

$m_{total-S}$	= total amount of mercury in sample	=	7.9536	µg
$m_{T-B-allow}$	= total allowable blank correction	=	0.0000	µg
m_n	= total mercury in sample corrected for allowable blank	=	7.9536	µg

5. Sample corrected for allowable blank - Prorated for each fraction (µg)

$$m_{n-i} = \left(\frac{m_{i-S}}{m_{total-S}} \right) (m_n)$$

Where:

m_n	= total mercury in sample corrected for allowable blank	=	7.9536	µg
m_{1b-S}	= mercury amount in sample for Fraction 1b	=	<0.1000	µg
m_{2b-S}	= mercury amount in sample for Fraction 2b	=	7.9536	µg
m_{3a-S}	= mercury amount in sample for Fraction 3a	=	<0.2000	µg
m_{3b-S}	= mercury amount in sample for Fraction 3b	=	<0.5000	µg
m_{3c-S}	= mercury amount in sample for Fraction 3c	=	<0.4000	µg
$m_{total-S}$	= total amount of mercury in sample	=	7.9536	µg
m_{n-1b}	= mercury corrected for blank - prorated for Fraction 1b	=	<0.1000	µg
m_{n-2b}	= mercury corrected for blank - prorated for Fraction 2b	=	7.9536	µg
m_{n-3a}	= mercury corrected for blank - prorated for Fraction 3a	=	<0.2000	µg
m_{n-3b}	= mercury corrected for blank - prorated for Fraction 3b	=	<0.5000	µg
m_{n-3c}	= mercury corrected for blank - prorated for Fraction 3c	=	<0.4000	µg

**USEPA Method 29
 Mercury Sample Calculations**

Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

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 J_N

1. Mercury concentration (lb/dscf)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{2.205 \times 10^{-3}}{10^6} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 7.9536 μg
V_{mstd}	= volume metered, standard (dscf)	= 79.4277 dscf
2.205×10^{-3}	= conversion factor (lb/g)	= 2.205E-03 lb/g
10^6	= conversion factor ($\mu\text{g/g}$)	= 1.0E+06 $\mu\text{g/g}$
C_{sd}	= mercury concentration (lb/dscf)	= 2.2080E-10 lb/dscf

2. Mercury concentration ($\mu\text{g/dscm}$)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}} \right) (35.31)$$

Where:

m_n	= mercury collected in sample (total μg)	= 7.9536 μg
V_{mstd}	= volume metered, standard (dscf)	= 79.4277 dscf
35.31	= conversion factor (dscf/dscm)	= 35.31 dscf/dscm
C_{sd}	= mercury concentration ($\mu\text{g/dscm}$)	= 3.5358E+00 $\mu\text{g/dscm}$

3. Mercury concentration (mg/dscm)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{35.31}{1000} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 7.9536 μg
V_{mstd}	= volume metered, standard (dscf)	= 79.4277 dscf
35.31	= conversion factor (dscf/dscm)	= 35.31 dscf/dscm
1000	= conversion factor ($\mu\text{g/mg}$)	= 1000 $\mu\text{g/mg}$
C_{sd}	= mercury concentration (mg/dscm)	= 3.5358E-03 mg/dscm

4. Mercury concentration ($\mu\text{g}/\text{Nm}^3$ dry)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}} \right) (35.31) \left(\frac{68 + 460}{32 + 460} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 7.9536	μg
V_{mstd}	= volume metered, standard (dscf)	= 79.4277	dscf
35.31	= conversion factor (dscf/dscm)	= 35.31	dscf/dscm
68	= standard temperature ($^{\circ}\text{F}$)	= 68	$^{\circ}\text{F}$
32	= normal temperature ($^{\circ}\text{F}$)	= 32	$^{\circ}\text{F}$
460	= $^{\circ}\text{F}$ to $^{\circ}\text{R}$ conversion constant	= 460	

C_{sd}	= mercury concentration ($\mu\text{g}/\text{Nm}^3$ dry)	= 3.7945E+00	$\mu\text{g}/\text{Nm}^3$ dry
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5. Mercury concentration corrected to x% oxygen (lb/dscf example)

$$C_{sdx} = C_{sd} \left(\frac{20.9 - x}{20.9 - O_2} \right)$$

Where:

C_{sd}	= mercury concentration (lb/dscf)	= 2.2080E-10	lb/dscf
x	= oxygen content of corrected gas (%)	= 7.0	%
O_2	= proportion of oxygen in the gas stream by volume (%)	= 10.7	%
20.9	= oxygen content of ambient air (%)	= 20.9	%
C_{sdx}	= mercury concentration corrected to x% oxygen (lb/dscf)	= 3.0188E-10	lb/dscf @ x% O_2

6. Mercury concentration corrected to y% carbon dioxide (lb/dscf example)

$$C_{sdy} = C_{sd} \left(\frac{y}{CO_2} \right)$$

Where:

C_{sd}	= mercury concentration (lb/dscf)	= 2.2080E-10	lb/dscf
y	= carbon dioxide content of corrected gas (%)	= 12.0	%
CO_2	= proportion of carbon dioxide in the gas stream by volume (%)	= 8.3	%
C_{sdy}	= mercury conc. corrected to y% carbon dioxide (lb/dscf)	= 3.2052E-10	lb/dscf @ y% CO_2

7. Mercury concentration at actual gas conditions (lb/acf example)

$$C_a = C_{sd} \left(\frac{Q_{std}}{Q_a} \right)$$

Where:

C_{sd}	= mercury concentration (lb/dscf)	= 2.2080E-10	lb/dscf
Q_{std}	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 100,911	dscfm
Q_a	= volumetric flow rate at actual conditions (acfm)	= 186,645	acfm
C_a	= mercury concentration at actual gas conditions (lb/acf)	= 1.1938E-10	lb/acf

8. Mercury emission rate (lb/hr)

$$E_{lb/hr} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{2.205 \times 10^{-3}}{10^6} \right) (Q_{std}) (60)$$

Where:

m_n	= mercury collected in sample (total μg)	= 7.9536 μg
V_{mstd}	= volume metered, standard (dscf)	= 79.4277 dscf
2.205×10^{-3}	= conversion factor (lb/g)	= 2.205E-03 lb/g
10^6	= conversion factor ($\mu\text{g/g}$)	= 1.0E+06 $\mu\text{g/g}$
Q_{std}	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 100,911 dscfm
60	= conversion factor (min/hr)	= 60 min/hr
$E_{lb/hr}$	= mercury emission rate (lb/hr)	= 1.3369E-03 lb/hr

9. Mercury emission rate (g/s)

$$E_{g/s} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{Q_{std}}{(10^6)(60)} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 7.9536 μg
V_{mstd}	= volume metered, standard (dscf)	= 79.4277 dscf
Q_{std}	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 100,911 dscfm
10^6	= conversion factor ($\mu\text{g/g}$)	= 1.0E+06 $\mu\text{g/g}$
60	= conversion factor (sec/min)	= 60 sec/min
$E_{g/s}$	= mercury emission rate (g/s)	= 1.6841E-04 g/s

10. Mercury emission rate (Ton/yr)

$$E_{T/yr} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{2.205 \times 10^{-3}}{10^6} \right) (Q_{std}) (60) \left(\frac{Cap}{2000} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 7.9536 μg
V_{mstd}	= volume metered, standard (dscf)	= 79.4277 dscf
2.205×10^{-3}	= conversion factor (lb/g)	= 2.205E-03 lb/g
10^6	= conversion factor ($\mu\text{g/g}$)	= 1.0E+06 $\mu\text{g/g}$
Q_{std}	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 100,911 dscfm
60	= conversion factor (min/hr)	= 60 min/hr
Cap	= capacity factor for process (hours operated/year)	= 8,760 hours/yr
2000	= conversion factor (lb/Ton)	= 2000 lb/Ton
$E_{T/yr}$	= mercury emission rate (Ton/yr)	= 5.8555E-03 Ton/yr

11. Mercury emission rate - Fd-based (lb/MMBtu)

$$E_{Fd} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{2.205 \times 10^{-3}}{10^6} \right) (F_d) \left(\frac{20.9}{20.9 - O_2} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 7.9536	μg
V_{mstd}	= volume metered, standard (dscf)	= 79.4277	dscf
2.205×10^{-3}	= conversion factor (lb/g)	= 2.205E-03	lb/g
10^6	= conversion factor ($\mu\text{g/g}$)	= 1.0E+06	$\mu\text{g/g}$
F_d	= ratio of gas volume to heat content of fuel (dscf/MMBtu)	= 9,570	dscf/MMBtu
O_2	= proportion of oxygen in the gas stream by volume (%)	= 10.7	%
20.9	= oxygen content of ambient air (%)	= 20.9	%
E_{Fd}	= mercury emission rate - Fd-based (lb/MMBtu)	= 4.3439E-06	lb/MMBtu

12. Mercury emission rate - Fc-based (lb/MMBtu)

$$E_{Fc} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{2.205 \times 10^{-3}}{10^6} \right) (F_c) \left(\frac{100}{CO_2} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 7.9536	μg
V_{mstd}	= volume metered, standard (dscf)	= 79.4277	dscf
2.205×10^{-3}	= conversion factor (lb/g)	= 2.205E-03	lb/g
10^6	= conversion factor ($\mu\text{g/g}$)	= 1.0E+06	$\mu\text{g/g}$
F_c	= ratio of gas volume to heat content of fuel (dscf/MMBtu)	= 1,820	dscf/MMBtu
CO_2	= proportion of oxygen in the gas stream by volume (%)	= 8.3	%
100	= conversion factor	= 100	
E_{Fc}	= mercury emission rate - Fc-based (lb/MMBtu)	= 4.8612E-06	lb/MMBtu

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WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-7

PARAMETERS

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Wheelabrator North Broward, Inc.
 Clean Air Project No: 10955
 Unit 3 FF Outlet

**USEPA Method 29 (Trace Metals)
 Sampling, Velocity and Moisture Parameters**

Run No.	1	2	3	Average
Date (2010)	Dec 8	Dec 8	Dec 8	
Start Time (approx.)	08:04	10:45	13:10	
Stop Time (approx.)	10:19	12:53	15:15	
Sampling Conditions				
V_d Dry gas meter correction factor	0.9960	0.9960	0.9960	
C_p Pitot tube coefficient	0.8200	0.8200	0.8200	
P_g Static pressure (in. H ₂ O)	-10.7000	-10.6000	-10.4000	
A_s Sample location area (ft ²)	64.0000	64.0000	64.0000	
P_{bar} Barometric pressure (in. Hg)	30.04	30.04	30.04	30.0400
D_n Nozzle diameter (in.)	0.2710	0.2710	0.2710	
O_2 Oxygen (dry volume %)	10.7333	10.7333	10.1333	10.5333
CO_2 Carbon dioxide (dry volume %)	8.2667	8.2000	8.9333	8.4667
N_2+CO Nitrogen plus carbon monoxide (dry volume %)	81.0000	81.0667	80.9333	81.0000
V_{lc} Total Liquid collected (ml)	416.50	395.10	392.00	
V_m Volume metered, meter conditions (ft ³)	76.6900	78.6200	77.7450	
T_m Dry gas meter temperature (°F)	51.1200	63.8000	78.4400	
T_s Sample temperature (°F)	305.8400	306.8400	309.0000	307.2267
ΔH Meter box orifice pressure drop (in. H ₂ O)	1.2232	1.2308	1.1676	
θ Total sampling time (min)	125.0	125.0	125.0	
Flow Results				
V_{wstd} Volume of water collected (ft ³)	19.6005	18.5934	18.4475	18.8805
V_{mstd} Volume metered, standard (dscf)	79.4277	79.4569	76.4245	78.4364
P_s Sample gas pressure, absolute (in. Hg)	29.2532	29.2606	29.2753	29.2630
P_v Vapor pressure, actual (in. Hg)	29.2532	29.2606	29.2753	29.2630
B_{wo} Moisture measured in sample (% by volume)	19.7928	18.9631	19.4446	19.4002
B_{ws} Saturated moisture content (% by volume)	100.0000	100.0000	100.0000	100.0000
B_w Actual water vapor in gas (% by volume)	19.7928	18.9631	19.4446	19.4002
$\sqrt{\Delta P}$ Velocity head ($\sqrt{in. H_2O}$)	0.7097	0.7122	0.6895	0.7038
M_d MW of sample gas, dry (lb/lb-mole)	29.7520	29.7413	29.8347	29.7760
M_s MW of sample gas, wet (lb/lb-mole)	27.4259	27.5148	27.5335	27.4914
V_s Velocity of sample (ft/sec)	48.6054	48.7267	47.2119	48.1813
%I Isokinetic sampling (%)	100.6687	99.5313	99.6247	99.9416
Q_a Volumetric flow rate, actual (acfm)	186,645	187,110	181,294	185,016
Q_s Volumetric flow rate, standard (scfm)	125,812	125,994	121,795	124,534
Q_{std} Volumetric flow rate, dry standard (dscfm)	100,911	102,101	98,113	100,375
Q_{std7} Volumetric flow rate, dry std@7%O ₂ (dscfm)	73,808	74,678	75,996	74,827
Q_a Volumetric flow rate, actual (acf/hr)	11,198,676	11,226,627	10,877,631	11,100,978
Q_s Volumetric flow rate, standard (scf/hr)	7,548,747	7,559,619	7,307,715	7,472,027
Q_{std} Volumetric flow rate, dry standard (dscf/hr)	6,054,636	6,126,080	5,886,756	6,022,490
Q_a Volumetric flow rate, actual (m ³ /hr)	317,153	317,945	308,061	314,386
Q_s Volumetric flow rate, standard (m ³ /hr)	213,785	214,093	206,959	211,612
Q_{std} Volumetric flow rate, dry standard (dry m ³ /hr)	171,471	173,494	166,716	170,560
Q_{std7} Volumetric flow rate, dry std@7%O ₂ (dry m ³ /hr)	125,416	126,896	129,135	127,149
Q_s Volumetric flow rate, normal (Nm ³ /hr)	199,209	199,496	192,848	197,184
Q_{std} Volumetric flow rate, dry normal (Nm ³ /hr)	159,780	161,665	155,349	158,931
Q_{std7} Volumetric flow rate, dry normal @7%O ₂ (Nm ³ /hr)	116,865	118,244	120,331	118,480

Comments:

Average includes 3 runs.

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Wheelabrator North Broward, Inc.
 Clean Air Project No: 10955
 Unit 3 FF Outlet

**USEPA Method 29
 Mercury (Hg) Emission Parameters**

Run No.	1	2	3	Average	
Date (2010)	Dec 8	Dec 8	Dec 8		
Start Time (approx.)	08:04	10:45	13:10		
Stop Time (approx.)	10:19	12:53	15:15		
Process Conditions					
R _p	Steam Production Rate - (Klbs/hour)	179.6	179.9	180.0	179.9
P ₁	SDA Outlet Temperature - (°F)	320	320	320	320
F _d	Oxygen-based F-factor (dscf/MMBtu)	9,570	9,570	9,570	9,570
F _c	Carbon dioxide-based F-factor (dscf/MMBtu)	1,820	1,820	1,820	1,820
Cap	Capacity factor (hours/year)	8,760	8,760	8,760	8,760
Gas Conditions					
O ₂	Oxygen (dry volume %)	10.7333	10.7333	10.1333	10.5333
CO ₂	Carbon dioxide (dry volume %)	8.2667	8.2000	8.9333	8.4667
T _s	Sample temperature (°F)	305.8400	306.8400	309.0000	307.2267
B _w	Actual water vapor in gas (% by volume)	19.7928	18.9631	19.4446	19.4002
Gas Flow Rate					
Q _a	Volumetric flow rate, actual (acfm)	186,645	187,110	181,294	185,016
Q _s	Volumetric flow rate, standard (scfm)	125,812	125,994	121,795	124,534
Q _{std}	Volumetric flow rate, dry standard (dscfm)	100,911	102,101	98,113	100,375
Q _{std7}	Volumetric flow rate, dry std@7%O ₂ (dscfm)	73,808	74,678	75,996	74,827
Q _a	Volumetric flow rate, actual (acf/hr)	11,198,676	11,226,627	10,877,631	11,100,978
Q _s	Volumetric flow rate, standard (scf/hr)	7,548,747	7,559,619	7,307,715	7,472,027
Q _{std}	Volumetric flow rate, dry standard (dscf/hr)	6,054,636	6,126,080	5,886,756	6,022,490
Q _a	Volumetric flow rate, actual (m ³ /hr)	317,153	317,945	308,061	314,386
Q _s	Volumetric flow rate, standard (m ³ /hr)	213,785	214,093	206,959	211,612
Q _{std}	Volumetric flow rate, dry standard (dry m ³ /hr)	171,471	173,494	166,716	170,560
Q _{std7}	Volumetric flow rate, dry std@7%O ₂ (dry m ³ /hr)	125,416	126,896	129,135	127,149
Q _s	Volumetric flow rate, normal (Nm ³ /hr)	199,209	199,496	192,848	197,184
Q _{std}	Volumetric flow rate, dry normal (Nm ³ /hr)	159,780	161,665	155,349	158,931
Q _{std7}	Volumetric flow rate, dry normal @7%O ₂ (Nm ³ /hr)	116,865	118,244	120,331	118,480
Sampling Data					
V _{std}	Volume metered, standard (dscf)	79.4277	79.4569	76.4245	78.4364
%I	Isokinetic sampling (%)	100.6687	99.5313	99.6247	99.9416
Laboratory Data					
m _{n-1b}	Fraction 1B Prorated (µg)	<0.1000	<0.1000	<0.1000	<0.1000
m _{n-2b}	Fraction 2B Prorated (µg)	7.9536	7.4497	10.7533	8.7189
m _{n-3a}	Fraction 3A Prorated (µg)	<0.2000	0.3763	<0.2000	<0.2588
m _{n-3b}	Fraction 3B Prorated (µg)	<0.5000	<0.5000	<0.5000	<0.5000
m _{n-3c}	Fraction 3C Prorated (µg)	<0.4000	<0.4000	<0.4000	<0.4000
m _n	Total matter corrected for allowable blanks (µg)	7.9536	7.8260	10.7533	8.8443
Mercury Results - Total					
C _{std}	Concentration (lb/dscf)	2.2080E-10	2.1718E-10	3.1026E-10	2.4941E-10
C _{std7}	Concentration @7% O ₂ (lb/dscf)	3.0188E-10	2.9693E-10	4.0055E-10	3.3312E-10
C _{std12}	Concentration @12% CO ₂ (lb/dscf)	3.2052E-10	3.1782E-10	4.1676E-10	3.5170E-10
C _a	Concentration (lb/acf)	1.1938E-10	1.1851E-10	1.6790E-10	1.3526E-10
C _{std}	Concentration (µg/dscm)	3.5358E+00	3.4778E+00	4.9683E+00	3.9940E+00
C _{std7}	Concentration @7% O ₂ (µg/dscm)	4.8342E+00	4.7549E+00	6.4142E+00	5.3344E+00
C _{std12}	Concentration @12% CO ₂ (µg/dscm)	5.1326E+00	5.0895E+00	6.6738E+00	5.6320E+00
C _{std}	Concentration (mg/dscm)	3.5358E-03	3.4778E-03	4.9683E-03	3.9940E-03
C _{std7}	Concentration @7% O ₂ (mg/dscm)	4.8342E-03	4.7549E-03	6.4142E-03	5.3344E-03
C _{std12}	Concentration @12% CO ₂ (mg/dscm)	5.1326E-03	5.0895E-03	6.6738E-03	5.6320E-03
C _a	Concentration (µg/m ³ (actual,wet))	1.9117E+00	1.8978E+00	2.6887E+00	2.1661E+00
C _{std}	Concentration (µg/Nm ³ dry)	3.7945E+00	3.7323E+00	5.3318E+00	4.2862E+00
C _{std7}	Concentration @7% O ₂ (µg/Nm ³ dry)	5.1879E+00	5.1028E+00	6.8835E+00	5.7248E+00
C _{std12}	Concentration @12% CO ₂ (µg/Nm ³ dry)	5.5082E+00	5.4619E+00	7.1622E+00	6.0441E+00
E _{lb/hr}	Rate (lb/hr)	1.3369E-03	1.3305E-03	1.8264E-03	1.4979E-03
E _{g/s}	Rate (g/s)	1.6841E-04	1.6761E-04	2.3008E-04	1.8870E-04
E _{T/yr}	Rate (Ton/yr)	5.8555E-03	5.8274E-03	7.9996E-03	6.5608E-03
E _{Fd}	Rate - Fd-based (lb/MMBtu)	4.3439E-06	4.2726E-06	5.7636E-06	4.7934E-06
E _{Fc}	Rate - Fc-based (lb/MMBtu)	4.8612E-06	4.8203E-06	6.3209E-06	5.3341E-06

Wheelabrator North Broward, Inc.
 Clean Air Project No: 10955
 Unit 3 FF Outlet

**USEPA Method 29
 Mercury (Hg) Emission Parameters (continued)
 Separate Front Half Results**

Run No.	1	2	3	Average
Date (2010)	Dec 8	Dec 8	Dec 8	
Start Time (approx.)	08:04	10:45	13:10	
Stop Time (approx.)	10:19	12:53	15:15	

Mercury Results - Front Half

C _{sd}	Concentration (lb/dscf)	<2.7761E-12	<2.7751E-12	<2.8852E-12	<2.8121E-12
C _{sd7}	Concentration @7% O ₂ (lb/dscf)	<3.7955E-12	<3.7941E-12	<3.7249E-12	<3.7715E-12
C _{sd12}	Concentration @12% CO ₂ (lb/dscf)	<4.0298E-12	<4.0611E-12	<3.8756E-12	<3.9889E-12
C _a	Concentration (lb/acf)	<1.5009E-12	<1.5143E-12	<1.5614E-12	<1.5255E-12
C _{sd}	Concentration (µg/dscm)	<4.4456E-02	<4.4439E-02	<4.6202E-02	<4.5032E-02
C _{sd7}	Concentration @7% O ₂ (µg/dscm)	<6.0780E-02	<6.0758E-02	<5.9648E-02	<6.0395E-02
C _{sd12}	Concentration @12% CO ₂ (µg/dscm)	<6.4532E-02	<6.5033E-02	<6.2063E-02	<6.3876E-02
C _{sd}	Concentration (mg/dscm)	<4.4456E-05	<4.4439E-05	<4.6202E-05	<4.5032E-05
C _{sd7}	Concentration @7% O ₂ (mg/dscm)	<6.0780E-05	<6.0758E-05	<5.9648E-05	<6.0395E-05
C _{sd12}	Concentration @12% CO ₂ (mg/dscm)	<6.4532E-05	<6.5033E-05	<6.2063E-05	<6.3876E-05
C _a	Concentration (µg/m ³ (actual,wet))	<2.4035E-02	<2.4249E-02	<2.5004E-02	<2.4429E-02
C _{sd}	Concentration (µg/Nm ³ dry)	<4.7708E-02	<4.7691E-02	<4.9583E-02	<4.8327E-02
C _{sd7}	Concentration @7% O ₂ (µg/Nm ³ dry)	<6.5227E-02	<6.5204E-02	<6.4013E-02	<6.4815E-02
C _{sd12}	Concentration @12% CO ₂ (µg/Nm ³ dry)	<6.9254E-02	<6.9791E-02	<6.6604E-02	<6.8550E-02
E _{lb/hr}	Rate (lb/hr)	<1.6808E-05	<1.7000E-05	<1.6984E-05	<1.6931E-05
E _{g/s}	Rate (g/s)	<2.1175E-06	<2.1416E-06	<2.1396E-06	<2.1329E-06
E _{T/yr}	Rate (Ton/yr)	<7.3620E-05	<7.4462E-05	<7.4392E-05	<7.4158E-05
E _{Fd}	Rate - Fd-based (lb/MMBtu)	<5.4616E-08	<5.4595E-08	<5.3599E-08	<5.4270E-08
E _{Fc}	Rate - Fc-based (lb/MMBtu)	<6.1119E-08	<6.1593E-08	<5.8781E-08	<6.0498E-08

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Wheelabrator North Broward, Inc.
 Clean Air Project No: 10955
 Unit 3 FF Outlet

**USEPA Method 29
 Mercury (Hg) Emission Parameters (continued)
 Separate Impinger 1-3 Results**

Run No.	1	2	3	Average
Date (2010)	Dec 8	Dec 8	Dec 8	
Start Time (approx.)	08:04	10:45	13:10	
Stop Time (approx.)	10:19	12:53	15:15	

Mercury Results - Impingers 1-3 Solution

C _{ad}	Concentration (lb/dscf)	2.2080E-10	2.0674E-10	3.1026E-10	2.4593E-10
C _{ad7}	Concentration @7% O ₂ (lb/dscf)	3.0188E-10	2.8265E-10	4.0055E-10	3.2836E-10
C _{ad12}	Concentration @12% CO ₂ (lb/dscf)	3.2052E-10	3.0254E-10	4.1676E-10	3.4661E-10
C _a	Concentration (lb/acf)	1.1938E-10	1.1281E-10	1.6790E-10	1.3336E-10
C _{ad}	Concentration (µg/dscm)	3.5358E+00	3.3106E+00	4.9683E+00	3.9382E+00
C _{ad7}	Concentration @7% O ₂ (µg/dscm)	4.8342E+00	4.5263E+00	6.4142E+00	5.2582E+00
C _{ad12}	Concentration @12% CO ₂ (µg/dscm)	5.1326E+00	4.8447E+00	6.6738E+00	5.5504E+00
C _{ad}	Concentration (mg/dscm)	3.5358E-03	3.3106E-03	4.9683E-03	3.9382E-03
C _{ad7}	Concentration @7% O ₂ (mg/dscm)	4.8342E-03	4.5263E-03	6.4142E-03	5.2582E-03
C _{ad12}	Concentration @12% CO ₂ (mg/dscm)	5.1326E-03	4.8447E-03	6.6738E-03	5.5504E-03
C _a	Concentration (µg/m ³ (actual,wet))	1.9117E+00	1.8065E+00	2.6887E+00	2.1356E+00
C _{ad}	Concentration (µg/Nm ³ dry)	3.7945E+00	3.5528E+00	5.3318E+00	4.2264E+00
C _{ad7}	Concentration @7% O ₂ (µg/Nm ³ dry)	5.1879E+00	4.8575E+00	6.8835E+00	5.6430E+00
C _{ad12}	Concentration @12% CO ₂ (µg/Nm ³ dry)	5.5082E+00	5.1992E+00	7.1622E+00	5.9565E+00
E _{lb/hr}	Rate (lb/hr)	1.3369E-03	1.2665E-03	1.8264E-03	1.4766E-03
E _{g/s}	Rate (g/s)	1.6841E-04	1.5955E-04	2.3008E-04	1.8601E-04
E _{T/yr}	Rate (Ton/yr)	5.8555E-03	5.5472E-03	7.9996E-03	6.4674E-03
E _{Fd}	Rate - Fd-based (lb/MMBtu)	4.3439E-06	4.0672E-06	5.7636E-06	4.7249E-06
E _{Fc}	Rate - Fc-based (lb/MMBtu)	4.8612E-06	4.5885E-06	6.3209E-06	5.2569E-06

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Wheelabrator North Broward, Inc.
 Clean Air Project No: 10955
 Unit 3 FF Outlet

**USEPA Method 29
 Mercury (Hg) Emission Parameters (continued)
 Separate Impinger 4 Results**

Run No.	1	2	3	Average
Date (2010)	Dec 8	Dec 8	Dec 8	
Start Time (approx.)	08:04	10:45	13:10	
Stop Time (approx.)	10:19	12:53	15:15	
Mercury Results - Impinger 4 Solution				
C _{sd} Concentration (lb/dscf)	<5.5522E-12	1.0443E-11	<5.7704E-12	<7.2554E-12
C _{sd7} Concentration @7% O ₂ (lb/dscf)	<7.5911E-12	1.4278E-11	<7.4497E-12	<9.7731E-12
C _{sd12} Concentration @12% CO ₂ (lb/dscf)	<8.0597E-12	1.5283E-11	<7.7513E-12	<1.0365E-11
C _s Concentration (lb/acf)	<3.0018E-12	5.6987E-12	<3.1228E-12	<3.9411E-12
C _{sd} Concentration (µg/dscm)	<8.8911E-02	1.6724E-01	<9.2405E-02	<1.1618E-01
C _{sd7} Concentration @7% O ₂ (µg/dscm)	<1.2156E-01	2.2865E-01	<1.1930E-01	<1.5650E-01
C _{sd12} Concentration @12% CO ₂ (µg/dscm)	<1.2906E-01	2.4474E-01	<1.2413E-01	<1.6598E-01
C _{sd} Concentration (mg/dscm)	<8.8911E-05	1.6724E-04	<9.2405E-05	<1.1618E-04
C _{sd7} Concentration @7% O ₂ (mg/dscm)	<1.2156E-04	2.2865E-04	<1.1930E-04	<1.5650E-04
C _{sd12} Concentration @12% CO ₂ (mg/dscm)	<1.2906E-04	2.4474E-04	<1.2413E-04	<1.6598E-04
C _s Concentration (µg/m ³ (actual,wet))	<4.8070E-02	9.1257E-02	<5.0008E-02	<6.3112E-02
C _{sd} Concentration (µg/Nm ³ dry)	<9.5417E-02	1.7947E-01	<9.9166E-02	<1.2469E-01
C _{sd7} Concentration @7% O ₂ (µg/Nm ³ dry)	<1.3045E-01	2.4538E-01	<1.2803E-01	<1.6795E-01
C _{sd12} Concentration @12% CO ₂ (µg/Nm ³ dry)	<1.3851E-01	2.6265E-01	<1.3321E-01	<1.7812E-01
E _{sd/hr} Rate (lb/hr)	<3.3617E-05	6.3978E-05	<3.3969E-05	<4.3854E-05
E _{sd/s} Rate (g/s)	<4.2349E-06	8.0597E-06	<4.2793E-06	<5.5246E-06
E _{sd/yr} Rate (Ton/yr)	<1.4724E-04	2.8022E-04	<1.4878E-04	<1.9208E-04
E _{Fd} Rate - Fd-based (lb/MMBtu)	<1.0923E-07	2.0546E-07	<1.0720E-07	<1.4063E-07
E _{Fc} Rate - Fc-based (lb/MMBtu)	<1.2224E-07	2.3179E-07	<1.1756E-07	<1.5720E-07

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**USEPA Method 29
 Mercury (Hg) Emission Parameters (continued)
 Separate Impinger 5-6 Results**

Run No.	1	2	3	Average
Date (2010)	Dec 8	Dec 8	Dec 8	
Start Time (approx.)	08:04	10:45	13:10	
Stop Time (approx.)	10:19	12:53	15:15	

Mercury Results - Filtered Permanganate Solution

C _{ad}	Concentration (lb/dscf)	<1.3881E-11	<1.3875E-11	<1.4426E-11	<1.4061E-11
C _{ad7}	Concentration @7% O ₂ (lb/dscf)	<1.8978E-11	<1.8971E-11	<1.8624E-11	<1.8858E-11
C _{ad12}	Concentration @12% CO ₂ (lb/dscf)	<2.0149E-11	<2.0306E-11	<1.9378E-11	<1.9944E-11
C _a	Concentration (lb/acf)	<7.5046E-12	<7.5715E-12	<7.8071E-12	<7.6277E-12
C _{ad}	Concentration (µg/dscm)	<2.2228E-01	<2.2220E-01	<2.3101E-01	<2.2516E-01
C _{ad7}	Concentration @7% O ₂ (µg/dscm)	<3.0390E-01	<3.0379E-01	<2.9824E-01	<3.0198E-01
C _{ad12}	Concentration @12% CO ₂ (µg/dscm)	<3.2266E-01	<3.2516E-01	<3.1032E-01	<3.1938E-01
C _{ad}	Concentration (mg/dscm)	<2.2228E-04	<2.2220E-04	<2.3101E-04	<2.2516E-04
C _{ad7}	Concentration @7% O ₂ (mg/dscm)	<3.0390E-04	<3.0379E-04	<2.9824E-04	<3.0198E-04
C _{ad12}	Concentration @12% CO ₂ (mg/dscm)	<3.2266E-04	<3.2516E-04	<3.1032E-04	<3.1938E-04
C _a	Concentration (µg/m ³ (actual,wet))	<1.2018E-01	<1.2125E-01	<1.2502E-01	<1.2215E-01
C _{ad}	Concentration (µg/Nm ³ dry)	<2.3854E-01	<2.3845E-01	<2.4792E-01	<2.4164E-01
C _{ad7}	Concentration @7% O ₂ (µg/Nm ³ dry)	<3.2614E-01	<3.2602E-01	<3.2006E-01	<3.2407E-01
C _{ad12}	Concentration @12% CO ₂ (µg/Nm ³ dry)	<3.4627E-01	<3.4896E-01	<3.3302E-01	<3.4275E-01
E _{lb/hr}	Rate (lb/hr)	<8.4042E-05	<8.5002E-05	<8.4922E-05	<8.4655E-05
E _{g/s}	Rate (g/s)	<1.0587E-05	<1.0708E-05	<1.0698E-05	<1.0665E-05
E _{T/yr}	Rate (Ton/yr)	<3.6810E-04	<3.7231E-04	<3.7196E-04	<3.7079E-04
E _{Fd}	Rate - Fd-based (lb/MMBtu)	<2.7308E-07	<2.7298E-07	<2.6799E-07	<2.7135E-07
E _{Fc}	Rate - Fc-based (lb/MMBtu)	<3.0560E-07	<3.0797E-07	<2.9390E-07	<3.0249E-07

Mercury Results - HCl Rinse + HCl/MnO2 Precipitate

C _{ad}	Concentration (lb/dscf)	<1.1104E-11	<1.1100E-11	<1.1541E-11	<1.1249E-11
C _{ad7}	Concentration @7% O ₂ (lb/dscf)	<1.5182E-11	<1.5177E-11	<1.4899E-11	<1.5086E-11
C _{ad12}	Concentration @12% CO ₂ (lb/dscf)	<1.6119E-11	<1.6244E-11	<1.5503E-11	<1.5955E-11
C _a	Concentration (lb/acf)	<6.0037E-12	<6.0572E-12	<6.2457E-12	<6.1022E-12
C _{ad}	Concentration (µg/dscm)	<1.7782E-01	<1.7776E-01	<1.8481E-01	<1.8013E-01
C _{ad7}	Concentration @7% O ₂ (µg/dscm)	<2.4312E-01	<2.4303E-01	<2.3859E-01	<2.4158E-01
C _{ad12}	Concentration @12% CO ₂ (µg/dscm)	<2.5813E-01	<2.6013E-01	<2.4825E-01	<2.5550E-01
C _{ad}	Concentration (mg/dscm)	<1.7782E-04	<1.7776E-04	<1.8481E-04	<1.8013E-04
C _{ad7}	Concentration @7% O ₂ (mg/dscm)	<2.4312E-04	<2.4303E-04	<2.3859E-04	<2.4158E-04
C _{ad12}	Concentration @12% CO ₂ (mg/dscm)	<2.5813E-04	<2.6013E-04	<2.4825E-04	<2.5550E-04
C _a	Concentration (µg/m ³ (actual,wet))	<9.6141E-02	<9.6997E-02	<1.0002E-01	<9.7718E-02
C _{ad}	Concentration (µg/Nm ³ dry)	<1.9083E-01	<1.9076E-01	<1.9833E-01	<1.9331E-01
C _{ad7}	Concentration @7% O ₂ (µg/Nm ³ dry)	<2.6091E-01	<2.6081E-01	<2.5605E-01	<2.5926E-01
C _{ad12}	Concentration @12% CO ₂ (µg/Nm ³ dry)	<2.7702E-01	<2.7917E-01	<2.6642E-01	<2.7420E-01
E _{lb/hr}	Rate (lb/hr)	<6.7233E-05	<6.8002E-05	<6.7938E-05	<6.7724E-05
E _{g/s}	Rate (g/s)	<8.4698E-06	<8.5666E-06	<8.5586E-06	<8.5317E-06
E _{T/yr}	Rate (Ton/yr)	<2.9448E-04	<2.9785E-04	<2.9757E-04	<2.9663E-04
E _{Fd}	Rate - Fd-based (lb/MMBtu)	<2.1846E-07	<2.1838E-07	<2.1439E-07	<2.1708E-07
E _{Fc}	Rate - Fc-based (lb/MMBtu)	<2.4448E-07	<2.4637E-07	<2.3512E-07	<2.4199E-07

122110 120748
 JPL @_N

WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-7

QA/QC DATA

D

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Nozzle Calibration Sheet

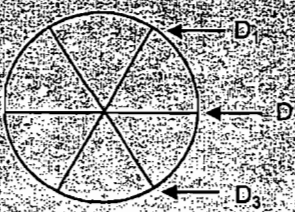
Client <i>wheelabrator</i>	Project Number <i>10955</i>
Calibrated by <i>C. Slomp</i>	Unit <i>5</i>
Date <i>12/17/10</i>	Runs <i>1</i>

Nozzle Identification	D ₁ (inches)	D ₂ (inches)	D ₃ (inches)	ΔD (inches)	D _{ave} (inches)
<i>271-1</i>	<i>0.272</i>	<i>0.271</i>	<i>0.271</i>	<i>0.001</i>	<i>0.271</i>

D₁, D₂, D₃ = three nozzle diameter measurements

ΔD = maximum difference between any two diameters
ΔD = 0.004 inches

D_{ave} = average of D₁, D₂, D₃



* (40 CFR 60, Appendix A, Method 5, Section 5.1)

QA/QC *CS*
Date *12/18/10*



Meter Box Full Test Calibration

Meter Box No: 61-6

Date of Calibration: 7/20/2010

Meter Box Y_d : 0.9960

Calibration Conducted by: Martin Vaquero

Meter Box $\Delta H@$: 1.7601

Signature: *Martin Vaquero*

Barometric Pressure: 29.23

				Standard Meter Gas Volume (ft ³)			Meter Box Gas Volume (ft ³)			Std. Meter Temperature (°F)			Meter Box Temperature (°F)			Time (min.)	Calibration Results	
Q	ΔH	ΔP	Y_{ds}	Initial	Final	V_{ds} Net	Initial	Final	V_d Net	T_{is} In	T_{os} Out	T_{ds} Avg.	T_i In	T_o Out	T_d Avg.	Θ	Y_d	$\Delta H@$
0.967	3.00	-1.90	1.0000	0.000	10.000	10.000	821.383	831.452	10.069	77.0	77.0	77.00	91.0	81.0	86.00	9.93	0.9974	1.7208
0.965	3.00	-1.90	1.0000	0.000	10.000	10.000	831.452	841.541	10.089	77.0	77.0	77.00	91.0	81.0	86.00	9.95	0.9955	1.7277
0.385	0.50	-1.10	1.0000	0.000	5.000	5.000	851.319	856.360	5.041	77.0	77.0	77.00	82.0	79.0	80.50	12.48	0.9943	1.8188
0.385	0.50	-1.10	1.0000	0.000	5.000	5.000	856.360	861.399	5.039	77.0	77.0	77.00	82.0	79.0	80.50	12.48	0.9947	1.8188
0.681	1.50	-1.40	1.0000	0.000	10.000	10.000	865.118	875.175	10.057	77.0	77.0	77.00	86.0	79.0	82.50	14.09	0.9972	1.7387
0.681	1.50	-1.40	1.0000	0.000	10.000	10.000	875.175	885.258	10.081	77.0	77.0	77.00	87.0	80.0	83.50	14.09	0.9967	1.7355
Averages																	0.99597	1.76006

D-4

Nomenclature	Equations
<p>P_b Barometric Pressure (in. Hg)</p> <p>Q Flow Rate (cfm)</p> <p>ΔH Orifice Pressure differential (in. H₂O)</p> <p>ΔP Inlet Pressure Differential (in. H₂O)</p> <p>V_d Gas Meter Volume - Dry (ft³)</p> <p>V_{ds} Standard Meter Volume - Dry (ft³)</p> <p>T_d Average Meter Box Temperature (°F)</p> <p>T_o Outlet Meter Box Temperature (°F)</p> <p>T_{ds} Average Standard Meter Temperature (°F)</p> <p>Y_d Meter Correction Factor (unitless), $Y_1 \leq Y_{avg} \pm 0.02$</p> <p>$Y_{ds}$ Standard Meter Correction Factor (unitless)</p> <p>$\Delta H@$ Orifice Pressure Differential giving 0.75 cfm of air at 68°F and 29.92 in. Hg (in. H₂O) $\Delta H@ \leq \Delta H@_{avg} \pm 0.2$</p> <p>$\Theta$ Duration of Run (minutes)</p>	$Y_d = (Y_{ds}) \left[\frac{V_{ds}}{V_d} \right] \left[\frac{T_d + 460}{T_{ds} + 460} \right] \left[\frac{P_b + \Delta P / 13.6}{P_b + \Delta H / 13.6} \right]$ $\Delta H@ = \frac{(0.0319)(\Delta H)}{P_b(T_o + 460)} \left[\frac{(T_{ds} + 460)\Theta}{(V_{ds})(Y_{ds})} \right]^2$ $Q = \frac{17.64(V_{ds})(P_b)}{(T_{ds} + 460)(\Theta)}$

Standard (in. Hg)	Gauge (in. Hg)
5.5	5.0
10.8	10.0
15.6	15.0
20.5	20.0
24.0	24.0

Meter Box - Pyrometer Calibration Sheet

Meter Box No: 61-6

Office: _____

Calibrated by: Martin Vaquero

Client: _____

Date: 7/20/10

Job No: _____

Temperature Scale Used: Fahrenheit

Type of Calibration: Full-Test

Calibration Reference Settings (°F)	Pyrometer Reading for each Channel (°F)						
	1	2	3	4	5	6	7
	Stack	Probe	Filter	Imp Out	Aux	DGM In	DGM Out
50	48	50	51				
100	98	99	100				
150	149	150	150				
200	199	199	200				
250	249	249	250				
300	299	299	300				
350	348	349	350				
400	398	399	400				
450	448	449	450				
500	499	499	500				
550	548	549	550				
600	598	599	600				

Tolerance = $\pm 2^{\circ}\text{F}$ difference from reference setting.

Calibration Reference Information

Reference Used: <u>Omega CL23A</u>	Serial No: <u>T-279500</u>
Calibrated By: <u>JH Metrology</u>	Exp. Date: <u>8/18/2010</u>
Calibration Report No: <u>R044791</u>	

Meter Box Critical Orifice Post-Test Calibration Data

Project No. 10955 Meter No. 61-6 Orifice C-4
 Location Warehouse Meter Yd 0.9960 Orifice K' 0.4763
 Test Date 12/15/2010 Meter ΔH@ 1.7601 Orifice Cal. Date 11/30/10
 Operator G. Pavlovics Full Test Cal. Date 07/20/10

Leak Checks

Negative Pressure Pass
No movement of manometer in one-minute

Positive Pressure Pass
No movement of manometer in one-minute

Important: All leak checks must pass in order for calibration to be valid.

Barom. Press. (P_b) 29.00 in. Hg

Run	Elapsed Time (minutes)	Meter Volume (dcf)	Meter Temperature		Ambient Temp. (°F)	Orifice ΔH (in. W.C.)	Vacuum (in. Hg)	Net Run Time - θ (minutes)	Net Meter Volume for Run - V _m (dcf)	Avg. Meter Temp. for Run T _m (°F)	DGM Calibration Factor - Y _i	Percent Variation - ΔY _i
			Inlet (°F)	Outlet (°F)								
	0.0	705.80	66	64								
1	5.0	708.91	66	64	69	1.20	19	5.0	3.11	65.0	0.9879	-0.4%
2	10.0	712.01	67	65	69	1.10	19	5.0	3.10	65.5	0.9923	0.0%
3	15.0	715.10	68	65	69	1.10	19	5.0	3.09	66.3	0.9969	0.5%
											Average Y _i	0.9923
											Cal. Error	-0.4%

Calculations and Specifications

$$Y_i = \frac{K' \times P_b \times (T_m + 460) \times \theta}{17.64 \times V_m \times (P_b + \Delta H / 13.6) \times \sqrt{T_{amb} + 460}}$$

$$\Delta Y_i = \frac{Y_i - \bar{Y}_i}{\bar{Y}_i} \times 100 \quad \text{Spec.: } \Delta Y_i \leq \pm 2\%$$

$$\text{Cal. Error} = \frac{\bar{Y}_i - Y_d}{Y_d} \times 100 \quad \text{Spec.: } \text{Cal. Error} \leq \pm 5\%$$

Sample Probe Calibration

Probe Type: M5 with S-Type Pitot I.D. Number: 67-8-18
 Project Number: _____

Thermocouple Calibration

Reference Type: Thermocouple Reference I.D. No: 15-078-39 Pyrometer I.D. No: 80512890 Units: *F

Point No.	Target Temp.	Reference Temp.	Indicated Temp.	Temp. Difference	% Difference*	Specification
1	Ambient	70	70	0	0.00%	%Difference ≤ 1.5
2	200°F-250°F	218	217	1	0.15%	

* Based on Absolute Temperature (Rankine)

Does thermocouple assembly meet specifications? → YES

Pitot Tube Calibration (Wind Tunnel Method @ 49 ft/sec)

Reference Pitot I.D. No: Wind Tunnel Reference Pitot Cp: 0.99

Pitot Side 'A':				Abs. Deviation	Specification Avg. Cp Deviations ≤ 0.01
Trial No.	Reference ΔP	Probe ΔP	Probe C _{p(S)} *	from Avg. C _{p(A)} **	
1	0.549	0.812	0.814	0.003	
2	0.561	0.816	0.820	0.003	
3	0.556	0.815	0.818	0.000	
Side 'A' Average Probe C _{p(A)} =			0.8175	0.0021	

Pitot Side 'B':				Abs. Deviation	Specification Avg. Cp Deviations ≤ 0.01
Trial No.	Reference ΔP	Probe ΔP	Probe C _{p(S)} *	from Avg. C _{p(B)} **	
1	0.554	0.802	0.823	0.000	
2	0.555	0.803	0.823	0.000	
3	0.556	0.805	0.823	0.000	
Side 'B' Average Probe C _{p(B)} =			0.8226	0.0000	

'A' Average C _p 0.817	—	'B' Average C _p 0.823	=	Difference -0.006	Specification Difference ≤ 0.01
-------------------------------------	---	-------------------------------------	---	----------------------	--------------------------------------

Does assembly meet specifications?

YES



If "Yes", C_p = Average of Side 'A' and 'B' Cp values. If "No", Pitot must be replaced.

$$C_{p(S)} = C_{p(STD)} \sqrt{\frac{\Delta P_{(STD)}}{\Delta P_{(S)}}}$$

$$** \text{ Deviation} = |C_{p(S)} - \overline{C_{p(A \text{ or } B)}}|$$

All specifications are from EPA-600/9-76-005, section 3.1

Probe Cp= 0.820 Calibrated by: R ARNOLD Date: 03/04/2010

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WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-7

FIELD DATA

E

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TEST LOCATION: FF outlet

Metals

TESTING

METHOD: 29 PAGE 1 OF 2

UNIT: 3

RUN: 1

FIELD DATA SHEET

Client: <u>Wheelerator</u>	Project No: <u>10955</u>
Plant: <u>N. Forward</u>	Date: <u>12/9/10</u>
Meter Operator: <u>K. Sullivan</u>	
Probe Operator: <u>N/A</u>	

Meter Box: <u>61-6</u>	Sample Box No: <u>M18</u>
Meter Yr: <u>0.9960</u>	Meter ΔH: <u>1.760i</u>
K Factor: <u>2.42</u>	Pitot C: <u>0.82</u>
Leak Rate Before: <u>0.004</u> [cfm] [Lpm] @ <u>15</u> (in. Hg)	
Leak Rate After: <u>0.002</u> [cfm] [Lpm] @ <u>6</u> (in. Hg)	
Pitot Leak Check Before: <input checked="" type="checkbox"/>	After: Good <input checked="" type="checkbox"/> Bad <input type="checkbox"/>

Cross-Section of Test Location

↑ [UP]

Duct Dimensions (in.): 96 x 96

Static Pres. (in. H ₂ O): <u>-10.7</u>	Port Len. (in.): <u>9.0</u>	Gas Flow (In) [Out]: <u>[Out]</u>	First point all the way of page: <u>[Out]</u>
---	-----------------------------	-----------------------------------	---

Amb. Temp (°F): <u>43</u>	Bar. Press: <u>30.04</u> [in. Hg] [mbar]
Probe I.D. No: <u>67-8-18</u>	
Liner Material: <u>PYREX</u>	

Filter No: <u>N/A</u>	
Thimble No: <u>N/A</u>	
Nozzle Diameter: <u>0.221</u>	Nozzle I.D.: <u>271-1</u>

Start Time: <u>8:04</u>	Stop Time: <u>10:19</u>
-------------------------	-------------------------

Transverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H ₂ O)	Orifice Setting ΔH (in. H ₂ O)	Gas Sample Volume V _m (L)	Stack Temp T _s (°F)	Probe T _p (°F)		Cond Temp T _c (°F)	DGM Inlet T _{m in} (°F)	DGM Outlet T _{m out} (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp T _t (°F)	Notes
						250	250						
1-1	5	0.30	0.73	460.50	304	250	249	48	42	41	3	N/A	9.7
2	10	0.28	0.68	462.75	294	253	241	51	42	41	3		10.5
3	15	0.40	0.97	465.46	305	253	250	51	45	41	3		10.3
4	20	0.55	1.3	468.57	307	250	250	51	46	42	4		9.4
5	25	0.55	1.3	471.77	308	250	249	53	48	42	4		10.0
2-1	30	0.63	1.5	476.17	307	247	251	55	48	43	4		9.8
2	35	0.55	1.3	479.31	306	250	250	58	51	44	4		9.8
3	40	0.57	1.21	482.57	306	253	250	59	53	45	4		10.0
4	45	0.54	1.3	485.74	307	251	251	60	52	45	4		10.7
5	50	0.48	1.2	488.73	305	249	249	61	55	46	4		9.9
3-1	55	0.68	1.6	493.08	306	248	250	62	54	47	5		9.8
2	60	0.521	1.3	496.29	307	250	250	64	57	48	4		9.9
	Total	17.7416	30.58	76.696	7646				1367	1189			
	Average	0.7087	1.2232	76.696	305.8100				57.1200				

Sum of square roots.

Circle correct bracketed units on data sheet.

QA/QC KS
Date 12/9/10

TEST LOCATION: FF outlet
 UNIT: 3 RUN: 1

Metals TESTING
 FIELD DATA SHEET

METHOD: 29 PAGE 2 OF 2

Client: Whelan Project No: 10955
 Plant: N. Howard Date: 12/5/10
 Meter Operator: KS
 Probe Operator: MA

Meter Box Sample Box No:
 Meter Yd Meter ΔH@:
 K Factor Pitot C:
 Leak Rate Before [cfm] [Lpm] @ (in. Hg)
 Leak Rate After [cfm] [Lpm] @ (in. Hg)
 Pitot Leak Check Before: After Good Bad

Cross-Section of Test Location

↑
 [N] [UP]

Duct Dimensions (in.):

Static Pres. (in. H ₂ O)	Port Len. (in.)	Gas Flow [In] [Out]	First point all the way of page [In] [Out]
-------------------------------------	-----------------	---------------------	--

Amb. Temp (°F) Bar Press. [in. Hg] [mbar]
 Probe I.D. No:
 Liner Material:

Filter No:
 Thimble No:
 Nozzle Diameter Nozzle I.D.:

Start Time Stop Time:

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H ₂ O)	Orifice Setting ΔH (in. H ₂ O)	Gas Sample Volume V _m Init. Vol. [L]	Stack Temp T _s (°F)	Probe T _p (°F)		Cond Temp T _c (°F)	DGM Inlet T _{m in} (°F)	DGM Outlet T _{m out} (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp T _t (°F)	Notes
						Set Points							
				496.29		250	250						
3-3	65	0.55	1.3	499.48	307	253	250	65	57	48	4	N/A	10.6
4	70	0.53	1.3	502.79	307	249	251	59	58	49	4		10.2 Perforated
5	75	0.51	1.2	505.72	300	249	249	53	59	50	4		10.5
4-1	80	0.51	1.2	508.79	305	248	250	50	58	50	4		10.9
2	85	0.59	1.4	512.12	308	247	248	50	59	50	4		10.3
3	90	0.53	1.3	515.30	307	250	253	59	59	51	4		10.6
4	95	0.48	1.2	518.36	307	252	250	48	60	51	4		10.8
5	100	0.48	1.2	521.42	307	249	249	48	60	51	4		10.6
5-1	105	0.49	1.2	525.15	303	249	250	49	59	52	4		10.8 Perforated
2	110	0.51	1.2	525.20	307	249	250	49	60	53	4		10.8 Perforated
3	115	0.51	1.2	531.27	307	250	252	49	61	53	4		10.6 0.25
4	120	0.48	1.2	534.29	307	251	250	50	61	53	4		10.5
5	125	0.45	1.1	537.260	306	250	250	57	61	53	4		10.2
	Total												
	Average												

Sum of square roots. Circle correct bracketed units on data sheet.



TEST LOCATION: FF outlet

Metals

TESTING

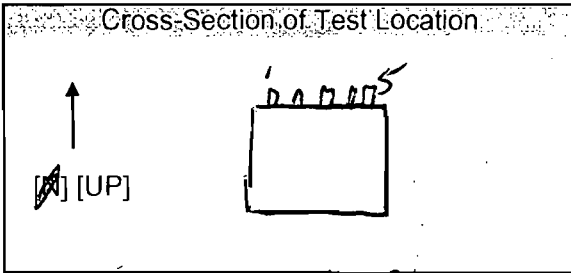
METHOD: 29 PAGE 1 OF 2

UNIT: 3

RUN: 2

FIELD DATA SHEET

Client: <u>Wheelabrator</u>	Project No: <u>10955</u>
Plant: <u>N Refinery</u>	Date: <u>12/8/10</u>
Meter Operator: <u>K Sullivan</u>	
Probe Operator: <u>N/A</u>	



Amb. Temp. (°F): <u>55</u>	Bar. Press: <u>30.04</u> [in Hg] [mbar]
Probe I.D. No: <u>27-8-15</u>	
Liner Material: <u>Pyrex</u>	

Meter Box: <u>61-6</u>	Sample Box No: <u>MM</u>
Meter Yr: <u>2006</u>	Meter ΔH: <u>1.701</u>
K Factor: <u>2.42</u>	Pilot C: <u>0.82</u>

Filter No: <u>N/A</u>	
Thimble No: <u>N/A</u>	
Nozzle Diameter: <u>2.271</u>	Nozzle I.D.: <u>291-1</u>

Leak Rate Before: <u>0.010</u> [scfm] [Lpm] @ <u>15</u> (in. Hg)
Leak Rate After: <u>0.004</u> [scfm] [Lpm] @ <u>6</u> (in. Hg)
Pilot Leak Check Before: <input checked="" type="checkbox"/> After: Good: <input checked="" type="checkbox"/> Bad: <input type="checkbox"/>

Duct Dimensions (in.): <u>96 x 96</u>			
Static Pres. (in. H ₂ O): <u>-10.6</u>	Port Len. (in.): <u>9.0</u>	Gas Flow [In] [Out] of page: <u>[In]</u>	First point all the way: <input checked="" type="checkbox"/> [Out]

Start Time: <u>10:45</u>	Stop Time: <u>12:53</u>
--------------------------	-------------------------

Traverse Point Number	Min/pl Elapsed Time	Velocity Head ΔP (in. H ₂ O)	Orifice Setting ΔH (in. H ₂ O)	Gas Sample Volume V _m Init. Vol. [L]	Stack Temp T _s (°F)	Probe/Filt. T _p (°F)		Cond. Temp T _c (°F)	DGM Inlet T _{min} (°F)	DGM Outlet T _{out} (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp (°F)	Notes
						250	250						
5-1	5	0.57	1.4	542.03	308	257	247	53	57	54	4	9.7	
2	10	0.55	1.3	545.23	307	249	247	49	59	55	4	10.3	
3	15	0.52	1.3	548.49	307	251	249	49	61	55	4	9.3	
4	20	0.50	1.2	551.25	307	251	251	52	63	56	4	10.7	
5	25	0.42	1.0	554.34	300	250	250	54	64	56	4	10.3	
4-1	30	0.53	1.3	557.52	307	250	250	54	65	57	4	10.7	
2	35	0.55	1.3	560.27	308	248	250	54	65	57	4	10.3	
3	40	0.53	1.3	563.98	308	251	250	53	65	58	4	10.5	
4	45	0.50	1.2	567.05	309	257	252	55	66	58	4	10.0	
5	50	0.46	1.1	570.00	306	250	250	58	66	58	4	11.0	
3-1	55	0.62	1.5	573.45	307	250	250	59	67	59	5	11.4	
2	60	0.57	1.4	576.82	308	249	250	60	68	59	5	11.2	
	Total	<u>12.5054</u>	<u>30.77</u>	<u>78.620</u>	<u>7621</u>				<u>1691</u>	<u>1499</u>			
	Average	<u>0.7122</u>	<u>1.2308</u>	<u>306.8400</u>	<u>306.8400</u>				<u>63.9000</u>				

Sum of square roots.

Circle correct bracketed units on data sheet.

QA/QC: KJ
Date: 12/8/10



TEST LOCATION: FF outbed

Metals TESTING

METHOD: 29 PAGE 2 OF 2

UNIT: 3 RUN: 2

FIELD DATA SHEET

Client: <u>Wheelabrator</u>	Project No.: <u>10955</u>
Plant: <u>N Braunschweig</u>	Date: <u>12/8/10</u>
Meter Operator: <u>KS</u>	
Probe Operator: <u>NA</u>	

Cross-Section of Test Location:

↑
[N] [UP]

Duct Dimensions (in.):

Static Pres (in. H ₂ O)	Port Len (in.)	Gas Flow [In] [Out]	First point all the way [In] [Out]
------------------------------------	----------------	---------------------	------------------------------------

of page

Amb. Temp (°F)	Bar. Press. [in. Hg] [mbar]
Probe I.D. No.	
Liner Material	

Meter Box	Sample Box No.
Meter Yr.	Meter ΔH _g
K Factor	Pitot C _p
Leak Rate Before [cfm] [Lpm] @ (in. Hg)	
Leak Rate After [cfm] [Lpm] @ (in. Hg)	
Pitot Leak Check Before: <input type="checkbox"/>	After: Good <input type="checkbox"/> Bad <input type="checkbox"/>

Filter No.	
Thimble No.	
Nozzle Diameter	Nozzle I.D.

Start Time	Stop Time
------------	-----------

Traverse Point Number	Min/pl Elapsed Time	Velocity Head ΔP (in. H ₂ O)	Orifice Setting ΔH (in. H ₂ O)	Gas Sample Volume V _m Init. Vol. [L]	Stack Temp T _s (°F)	Probe T _p (°F)		Filter T _f (°F)	Cond Temp T _c (°F)	DGM Inlet T _{m in} (°F)	DGM Outlet T _{m out} (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp T _t (°F)	Notes
						Set Points								
3-3	65	0.50	1.2	579.91	308	252	250	62	68	60	4	10.9		
4	70	0.47	1.1	582.55	308	250	250	65	69	60	4	10.6		
5	75	0.48	1.0	585.76	308	250	249	63	68	61	4	10.9		
2-1	81	0.65	1.6	589.32	307	249	251	55	68	61	5	11.3		
2	85	0.55	1.3	592.60	308	249	250	53	70	62	5	11.8		
3	90	0.57	1.4	595.99	311	252	251	50	70	62	5	11.2		
4	95	0.52	1.3	599.27	309	251	250	48	72	63	5	11.5		
5	100	0.50	1.2	602.40	308	249	250	48	72	63	5	11.5		
1-1	105	0.42	1.0	605.35	305	249	250	48	74	64	4	10.4		
2	110	0.42	1.0	608.25	301	249	248	48	74	65	4	11.5		
3	115	0.40	0.97	611.07	303	251	254	47	74	65	4	11.7		
4	120	0.47	1.1	614.08	306	250	251	48	73	65	4	11.6		
5	125	0.52	1.3	617.300	307	250	250	48	74	66	4	11.5		
Total														
Average														

Sum of square roots.

Circle correct bracketed units on data sheet.



TEST LOCATION: PF Outlet

UNIT: 3

RUN: 3

Metals

TESTING

METHOD: 29

PAGE 1

OF 2

FIELD DATA SHEET

Client: <u>Wheelabrator</u>	Project No.: <u>10955</u>
Plant: <u>N. Brown's</u>	Date: <u>12/8/10</u>
Meter Operator: <u>K. Sullivan</u>	
Probe Operator: <u>N/A</u>	

Meter Box: <u>61-6</u>	Sample Box No.: <u>M8</u>
Meter Yr: <u>0.9760</u>	Meter ΔH @: <u>1.722</u>
K Factor: <u>2.42</u>	Pitot Cp: <u>0.82</u>

Leak Rate Before: <u>0.003</u> [cfm] [Lpm] @ <u>12</u> (in. Hg)
Leak Rate After: <u>0.001</u> [cfm] [Lpm] @ <u>5</u> (in. Hg)
Pitot Leak Check: Before <input checked="" type="checkbox"/> After Good <input checked="" type="checkbox"/> Bad <input type="checkbox"/>

Cross-Section of Test Location			
Duct Dimensions (in.): <u>96 x 96</u>			
Static Pres (in. H ₂ O): <u>-10.4</u>	Port Len (in): <u>9.0</u>	Gas Flow (In) [Q _{in}] of page: <u>Q_{in}</u>	First point all the way (In) [Q _{out}]: <u>Q_{in}</u>

Amb. Temp (°F): <u>70</u>	Bar Press: <u>30.04</u> [Hg] [mbar]
Probe I.D. No: <u>67-8-18</u>	
Liner Material: <u>PYREX</u>	

Filter No: <u>N/A</u>		
Thimble No: <u>N/A</u>		
Nozzle Diameter: <u>0.221</u>	Nozzle I.D.: <u>221-1</u>	

Start Time: <u>13:10</u>	Stop Time: <u>15:15</u>
--------------------------	-------------------------

Inverse Point Number	Min/pl Elapsed Time	Velocity Head ΔP (in. H ₂ O)	Orifice Setting ΔH (in. H ₂ O)	Gas Sample Volume V _m Init. Vol. [L]	Stack Temp T _s (°F)	Probe T _p (°F)		Cond Temp T _c (°F)	DGM Inlet T _{min} (°F)	DGM Outlet T _{min} (°F)	Pump Vacuum (in. Hg)	XAD Tap Temp (°F)	Notes
						Set Points	Set Points						
	<u>5</u>			<u>618.165</u>		<u>250</u>	<u>250</u>						
<u>1-1</u>	<u>5</u>	<u>0.53</u>	<u>1.3</u>	<u>621.58</u>	<u>306</u>	<u>240</u>	<u>241</u>	<u>65</u>	<u>66</u>	<u>65</u>	<u>4</u>	<u>11.8</u>	
<u>2</u>	<u>10</u>	<u>0.45</u>	<u>1.1</u>	<u>624.54</u>	<u>300</u>	<u>252</u>	<u>252</u>	<u>64</u>	<u>73</u>	<u>67</u>	<u>3</u>	<u>11.9</u>	
<u>3</u>	<u>15</u>	<u>0.35</u>	<u>0.85</u>	<u>622.21</u>	<u>307</u>	<u>255</u>	<u>251</u>	<u>65</u>	<u>75</u>	<u>67</u>	<u>3</u>	<u>11.4</u>	
<u>4</u>	<u>20</u>	<u>0.45</u>	<u>1.1</u>	<u>630.30</u>	<u>307</u>	<u>252</u>	<u>250</u>	<u>56</u>	<u>76</u>	<u>68</u>	<u>4</u>	<u>11.0</u>	
<u>5</u>	<u>25</u>	<u>0.40</u>	<u>0.97</u>	<u>633.17</u>	<u>306</u>	<u>249</u>	<u>250</u>	<u>51</u>	<u>77</u>	<u>68</u>	<u>4</u>	<u>10.2</u>	
<u>2-1</u>	<u>30</u>	<u>0.60</u>	<u>1.5</u>	<u>636.75</u>	<u>307</u>	<u>249</u>	<u>250</u>	<u>49</u>	<u>79</u>	<u>69</u>	<u>5</u>	<u>11.0</u>	
<u>2</u>	<u>35</u>	<u>0.56</u>	<u>1.4</u>	<u>640.10</u>	<u>309</u>	<u>247</u>	<u>250</u>	<u>48</u>	<u>80</u>	<u>69</u>	<u>4</u>	<u>10.9</u>	
<u>3</u>	<u>40</u>	<u>0.50</u>	<u>1.2</u>	<u>643.20</u>	<u>309</u>	<u>252</u>	<u>251</u>	<u>48</u>	<u>80</u>	<u>70</u>	<u>4</u>	<u>10.8</u>	
<u>4</u>	<u>45</u>	<u>0.45</u>	<u>1.1</u>	<u>646.19</u>	<u>308</u>	<u>251</u>	<u>249</u>	<u>49</u>	<u>80</u>	<u>71</u>	<u>4</u>	<u>11.2</u>	
<u>5</u>	<u>50</u>	<u>0.37</u>	<u>0.90</u>	<u>648.97</u>	<u>307</u>	<u>250</u>	<u>250</u>	<u>49</u>	<u>82</u>	<u>71</u>	<u>3</u>	<u>11.4</u>	
<u>3-1</u>	<u>55</u>	<u>0.57</u>	<u>1.4</u>	<u>652.42</u>	<u>308</u>	<u>250</u>	<u>250</u>	<u>50</u>	<u>84</u>	<u>72</u>	<u>4</u>	<u>12.1</u>	
<u>2</u>	<u>60</u>	<u>0.50</u>	<u>1.2</u>	<u>655.57</u>	<u>309</u>	<u>247</u>	<u>249</u>	<u>51</u>	<u>86</u>	<u>73</u>	<u>4</u>	<u>12.1</u>	
	Total	<u>17.2377</u>	<u>29.19</u>	<u>77.745</u>	<u>7225</u>				<u>2080</u>	<u>1842</u>			
	Average	<u>0.6895</u>	<u>1.1626</u>	<u>77.745</u>	<u>309.0000</u>				<u>78.4400</u>				

Sum of square roots.

Circle correct bracketed units on data sheet.



TEST LOCATION: FF Outlet

Metals

TESTING

METHOD: 29 PAGE 2 OF 2

UNIT: 3

RUN: 3

FIELD DATA SHEET

Client: <u>Wheelabrator</u>	Project No: <u>10955</u>
Plant: <u>N. Towards</u>	Date: <u>12/8/10</u>
Meter Operator: <u>KS</u>	
Probe Operator: <u>MA</u>	

Meter Box	Sample Box No:
Meter Y ₀	Meter ΔH ₀
K Factor	Pitot C _p

Leak Rate Before	[cfm] [Lpm]	@	(in. Hg)
Leak Rate After	[cfm] [Lpm]	@	(in. Hg)
Pitot Leak Check Before	<input type="checkbox"/>	After: Good	<input type="checkbox"/> Bad <input type="checkbox"/>

Cross Section of Test Location

↑

[N] [UP]

Duct Dimensions (in.):

Static Pres (in. H ₂ O)	Port Len (in.)	Gas Flow [In] [Out]	First point all the way [In] [Out]
------------------------------------	----------------	---------------------	------------------------------------

of page

Amb. Temp (°F)	Bar. Press. [in. Hg] [mbar]
Probe I.D. No.	
Liner Material	

Filter No.	
Thimble No.	
Nozzle Diameter	Nozzle I.D.

Start Time	Stop Time
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Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H ₂ O)	Orifice Setting ΔH (in. H ₂ O)	Gas Sample Volume V _m Init. Vol. [L]	Stack Temp Ts (°F)	Probe T _p (°F)		Filter T _f (°F)	Cond Temp T _c (°F)	DGM Inlet T _{m in} (°F)	DGM Outlet T _{m out} (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp (°F) O ₂	Notes
						Set Points	Set Points							
3-3	65	0.47	1.1	655.51	310	252	250	52	87	74	4	11.3		
4	70	0.45	1.1	661.45	310	251	251	54	87	75	4	12.0		
5	75	0.45	1.2	664.45	310	250	250	55	87	76	4	12.1		
4-1	80	0.60	1.5	668.01	310	250	250	56	87	77	5	11.7		
2	85	0.55	1.3	671.29	310	246	249	53	88	78	4	11.5		
3	90	0.53	1.3	674.64	311	252	250	57	88	78	4	12.2		
4	95	0.48	1.2	677.78	311	251	250	51	87	78	4	13.0		
5	100	0.45	1.1	680.88	312	250	250	51	88	79	4	13.3		
5-1	105	0.48	1.2	683.97	309	249	250	52	89	79	4	13.0		
2	110	0.45	1.1	687.01	314	247	249	53	88	79	4	12.9		
3	115	0.45	1.1	690.03	312	252	250	53	88	79	4	12.7		
4	120	0.45	1.1	693.03	312	251	250	53	89	80	4	12.6		
5	125	0.40	0.97	695.916	311	249	249	54	89	80	4	12.5		
Total														
Average														

Sum of square roots.

Circle correct bracketed units on data sheet.



Impinger Weight Sheet

Client <i>Wheelabrator</i>	Unit Name / Location <i>3/FF Outlet</i>
Plant <i>N. Broward</i>	Job No. <i>10955</i> Method <i>29</i>

Balance Calibration	
Reference Weight ID <i>60151</i>	Reference Weight Reading <i>499.2</i>
Reference Weight Mass <i>460</i>	Reference Weight Mass must agree with Reference Weight Reading to within ±0.5 g.

Run No. <i>1</i>	Filter Type <i>Quartz</i>	Sample Box No. <i>M8</i>
Date <i>12/8/10</i>	Lot No. <i>-</i>	pH <i>-</i>
Analyst <i>C. Slimp</i>	Filter No. <i>R1</i>	Rinse <i>-</i>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	<i>Empty</i>	<i>607.7</i>	<i>415.7</i>	<i>192.0</i>	
Impinger 2	<i>100 mL 5% HNO₃ / 10% H₂O₂</i>	<i>665.5</i>	<i>545.3</i>	<i>140.2</i>	QA/QC CS Date <i>12/8/10</i>
Impinger 3	<i>ii</i>	<i>590.9</i>	<i>545.5</i>	<i>45.4</i>	
Impinger 4	<i>Empty</i>	<i>462.8</i>	<i>450.8</i>	<i>12.0</i>	
Impinger 5	<i>100 mL 4% KMnO₄ / 10% H₂SO₄</i>	<i>542.6</i>	<i>537.6</i>	<i>5.0</i>	Total Weight (gm)
Impinger 6	<i>ii</i>	<i>566.7</i>	<i>565.9</i>	<i>0.8</i>	<i>395.4</i>
Impinger 7	<i>Silica Gel</i>	<i>751.8</i>	<i>730.7</i>	<i>21.1</i>	<i>416.5</i>

Run No. <i>2</i>	Filter Type <i>Quartz</i>	Sample Box No. <i>M4</i>
Date <i>12/8/10</i>	Lot No. <i>-</i>	pH <i>-</i>
Analyst <i>C. Slimp</i>	Filter No. <i>R2</i>	Rinse <i>-</i>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	<i>Empty</i>	<i>606.4</i>	<i>428.8</i>	<i>177.6</i>	
Impinger 2	<i>100 mL 5% HNO₃ / 10% H₂O₂</i>	<i>730.5</i>	<i>621.1</i>	<i>109.4</i>	QA/QC CS Date <i>12/8</i>
Impinger 3	<i>ii</i>	<i>589.0</i>	<i>536.3</i>	<i>52.7</i>	
Impinger 4	<i>Empty</i>	<i>478.4</i>	<i>456.1</i>	<i>22.3</i>	
Impinger 5	<i>100 mL 4% KMnO₄ / 10% H₂SO₄</i>	<i>554.4</i>	<i>545.8</i>	<i>8.6</i>	Total Weight (gm)
Impinger 6	<i>ii</i>	<i>540.0</i>	<i>538.1</i>	<i>1.9</i>	<i>3382.5</i> <i>372.5</i>
Impinger 7	<i>Silica Gel</i>	<i>750.6</i>	<i>728.0</i>	<i>22.6</i>	<i>3405.1</i> <i>395.1</i>

Run No. <i>3</i>	Filter Type <i>Quartz</i>	Sample Box No. <i>M8</i>
Date <i>12/8/10</i>	Lot No. <i>-</i>	pH <i>-</i>
Analyst <i>C. Slimp</i>	Filter No. <i>R3</i>	Rinse <i>-</i>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	<i>Empty</i>	<i>695.6</i>	<i>419.2</i>	<i>276.4</i>	
Impinger 2	<i>100 mL 5% HNO₃ / 10% H₂O₂</i>	<i>629.5</i>	<i>546.7</i>	<i>82.8</i>	QA/QC CS Date <i>12/8</i>
Impinger 3	<i>ii</i>	<i>563.3</i>	<i>548.5</i>	<i>14.8</i>	
Impinger 4	<i>Empty</i>	<i>455.3</i>	<i>452.9</i>	<i>2.4</i>	
Impinger 5	<i>100 mL 4% KMnO₄ / 10% H₂SO₄</i>	<i>541.9</i>	<i>541.7</i>	<i>0.2</i>	Total Weight (gm)
Impinger 6	<i>ii</i>	<i>547.9</i>	<i>548.3</i>	<i>-0.4</i>	<i>3742</i> <i>376.2</i>
Impinger 7	<i>Silica Gel</i>	<i>767.3</i>	<i>751.5</i>	<i>15.8</i>	<i>410.0</i> <i>392.0</i>

FD50049-Impinger/Weight, August 2004
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QA/QC CS
Date *12/8/10*



ORSAT READINGS

TEST LOCATION: FF Outlet

PAGE 1 OF 1

Client <u>Wheelabrator</u>	Project Number <u>10955</u>	$F_o = \frac{20.9 - \%O_2}{\%CO_2}$
Plant <u>N. Browns</u>	Unit <u>3</u>	
Orsat ID <u>6</u>	Fuel Type <u>Waste</u>	Leak Check Passed <input checked="" type="checkbox"/>

Run Number	Method Number	Trial	Percent CO ₂	Percent O ₂ +CO ₂	Percent O ₂	F _o	Analyst	Analysis	
								Date	Time
1	29	1	8.2	19.0	10.8	1.23	C. Slimp	12/8	13:20
		2	8.2	19.0	10.8				
		3	8.4	19.0	10.6				
		Avg.	8.26		10.73				
2	29	1	8.2	19.0	10.8	1.23	C. Slimp	12/8	13:45
		2	8.2	19.0	10.8				
		3	8.2	18.8	10.6				
		Avg.	8.2		10.73				
3	29	1	9.0	19.2	10.4	1.18	C. Slimp	12/8	13:37
		2	8.8	19.0	10.2				
		3	9.0	19.0	10.0				
		Avg.	9.0	19.06	10.2				
		1							
		2							
		3							
		Avg.							
		1							
		2							
		3							
		Avg.							
		1							
		2							
		3							
		Avg.							

Repeat the analysis procedure until the results of any three analyses differ by no more than 0.2 percent by volume. Average the three acceptable values and report the results to the nearest 0.1 percent. Calculate F_o to verify results

Acceptable ranges for F_o :

Coal: Anthracite and Lignite	1.016-1.130	Gas: Natural	1.600-1.836
Bituminous	1.083-1.230	Propane	1.434-1.586
Oil: Distillate	1.260-1.413	Butane	1.405-1.553
Residual	1.210-1.370	Wood	1.000-1.120
Municipal Solid Waste	1.030-1.300	Wood Bark	1.003-1.130

FD003-Orsat v9, July 2008
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QA/QC ES
Date 12/8



WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-7

FIELD DATA PRINTOUTS

F

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Field Data Printout

Test Method: USEPA Method 29
Analyte: Trace Metals

Location: Unit 3 FF Outlet

Test Run: 1

Client: Wheelabrator North Broward, Inc.

Project No: 10955

Source Area (ft²): 64.00000

Meter Operator: _____
 Probe Operator: _____

Test Date: 12/08/10

Start Time: 08:04

Stop Time: 10:19

Leak Rate Before: 0.004 cfm @ 15 "Hg
 Leak Rate After: 0.002 cfm @ 6 "Hg

Bar. Press. (in. Hg): 30.04

Static P: -10.7

O₂ (dry volume %): 10.73

CO₂ (dry volume %): 8.27

N₂+CO (dry volume %): 81.00

Nozzle ID No: 271-1

Nozzle Diameter (D_n): 0.271

Probe ID No: 67-8-18

Pitot C_p: 0.8200

Pitot Leak Check: Pass Fail

H₂O (condensate, ml or gm): 395.4

H₂O (silica, g): 21.1

Actual Moisture (%): 19.79

Meter Box ID No: 61-6

Meter ΔH@: 1.76010

Meter Y_d: 0.99600

Traverse Point	Run Time 5.0 min/read	Pitot ΔP _s (in. H ₂ O)	Sample ΔH (in. H ₂ O)	Metered (dcf)	Stack T _s (°F)	Dry Gas Meter		√ΔP _s (calculated) (√in. H ₂ O)	Volume (calculated) (ft ³)	Isokinetics (calculated) (%)
						T _{m-in} (°F)	T _{m-out} (°F)			
	0.0			458.090						
1-01	5.0	0.30	0.73	460.500	304	42	41	0.55	2.41	104.2
1-02	10.0	0.28	0.68	462.750	294	42	41	0.53	2.25	100.0
1-03	15.0	0.40	0.97	465.460	305	45	41	0.63	2.71	101.3
1-04	20.0	0.55	1.30	468.570	307	46	42	0.74	3.11	99.1
1-05	25.0	0.55	1.30	471.770	308	48	42	0.74	3.20	101.9
LEAK CHECK	25.0			472.800						
2-01	30.0	0.63	1.50	476.170	307	48	43	0.79	3.37	100.1
2-02	35.0	0.55	1.30	479.310	306	51	44	0.74	3.14	99.3
2-03	40.0	0.57	1.40	482.570	306	53	45	0.75	3.26	101.0
2-04	45.0	0.54	1.30	485.740	307	54	45	0.73	3.17	100.9
2-05	50.0	0.48	1.20	488.730	305	55	46	0.69	2.99	100.6
LEAK CHECK	50.0			489.530						
3-01	55.0	0.68	1.60	493.080	306	54	47	0.82	3.55	100.5
3-02	60.0	0.54	1.30	496.290	307	57	48	0.73	3.21	101.6
3-03	65.0	0.55	1.30	499.480	307	57	48	0.74	3.19	100.0
3-04	70.0	0.53	1.30	502.780	307	58	49	0.73	3.30	105.2
3-05	75.0	0.51	1.20	505.720	306	59	50	0.71	2.94	95.3
4-01	80.0	0.51	1.20	508.790	305	58	50	0.71	3.07	99.5
4-02	85.0	0.59	1.40	512.120	308	59	50	0.77	3.33	100.5
4-03	90.0	0.53	1.30	515.300	307	59	51	0.73	3.18	101.1
4-04	95.0	0.48	1.20	518.360	307	60	51	0.69	3.06	102.1
4-05	100.0	0.48	1.20	521.420	307	60	51	0.69	3.06	102.1
LEAK CHECK	100.0			522.070						
5-01	105.0	0.49	1.20	525.150	303	59	52	0.70	3.08	101.4
5-02	110.0	0.51	1.20	528.200	307	60	53	0.71	3.05	98.5
5-03	115.0	0.51	1.20	531.270	307	61	53	0.71	3.07	99.0
5-04	120.0	0.48	1.20	534.290	307	61	53	0.69	3.02	100.4
5-05	125.0	0.45	1.10	537.260	306	61	53	0.67	2.97	101.9
Final	125.0		1.22320	76.69000	305.84000	51.12000		0.70967	76.69000	

25 points sampled

QC-Check: Field Averages

Sq.RLΔP	0.7097	1.2232	76.6900	305.8400	51.1200
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Avg. OK Avg. OK Avg. OK Avg. OK Avg. OK

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Field Data Printout

Test Method: USEPA Method 29
Analyte: Trace Metals

Location: Unit 3 FF Outlet
Test Run: 2
Client: Wheelabrator North Broward, Inc.
Project No: 10955
Source Area (ft²): 64.00000

Bar. Press. (in. Hg): 30.04
Static P: -10.6
O₂ (dry volume %): 10.73
CO₂ (dry volume %): 8.20
N₂+CO (dry volume %): 81.07

Nozzle ID No: 271-1
Nozzle Diameter (D_n): 0.271
Probe ID No: 67-8-18
Pitot C_p: 0.8200
Pitot Leak Check: Pass Fail

Meter Operator: _____
Probe Operator: _____

Test Date: 12/08/10
Start Time: 10:45
Stop Time: 12:53
Leak Rate Before: 0.010 cfm @ 15 "Hg
Leak Rate After: 0.004 cfm @ 6 "Hg

H₂O (condensate, ml or gm): 372.5
H₂O (silica, g): 22.6
Actual Moisture (%): 18.96

Meter Box ID. No: 61-6
Meter ΔH@: 1.76010
Meter Y_d: 0.99600

Traverse Point	Run Time 5.0 min/read	Pitot ΔP _s (in. H ₂ O)	Sample ΔH (in. H ₂ O)	Metered (dcf)	Stack T _s (°F)	Dry Gas Meter		√ΔP _s (calculated) (√in. H ₂ O)	Volume (calculated) (ft ³)	Isokinetics (calculated) (%)
						T _{m-in} (°F)	T _{m-out} (°F)			
	0.0			538.680						
5-01	5.0	0.57	1.40	542.030	308	57	54	0.75	3.35	101.7
5-02	10.0	0.55	1.30	545.230	307	59	55	0.74	3.20	98.6
5-03	15.0	0.52	1.30	548.410	307	61	55	0.72	3.18	100.5
5-04	20.0	0.50	1.20	551.450	307	63	56	0.71	3.04	97.7
5-05	25.0	0.42	1.00	554.340	300	64	56	0.65	2.89	100.7
4-01	30.0	0.53	1.30	557.520	307	65	57	0.73	3.18	99.0
4-02	35.0	0.55	1.30	560.770	308	65	57	0.74	3.25	99.4
4-03	40.0	0.53	1.30	563.980	308	65	58	0.73	3.21	99.9
4-04	45.0	0.50	1.20	567.050	309	66	58	0.71	3.07	98.3
4-05	50.0	0.46	1.10	570.000	306	66	58	0.68	2.95	98.3
3-01	55.0	0.62	1.50	573.450	307	67	59	0.79	3.45	99.0
3-02	60.0	0.57	1.40	576.820	308	68	59	0.75	3.37	100.8
3-03	65.0	0.50	1.20	579.910	308	68	60	0.71	3.09	98.5
3-04	70.0	0.47	1.10	582.850	308	68	60	0.69	2.94	96.7
3-05	75.0	0.42	1.00	585.760	308	68	61	0.65	2.91	101.1
2-01	80.0	0.65	1.60	589.320	307	68	61	0.81	3.56	99.5
2-02	85.0	0.55	1.30	592.600	308	70	62	0.74	3.28	99.4
2-03	90.0	0.57	1.40	595.990	311	70	62	0.75	3.39	101.1
2-04	95.0	0.52	1.30	599.270	309	72	63	0.72	3.28	102.0
2-05	100.0	0.50	1.20	602.400	308	72	63	0.71	3.13	99.1
1-01	105.0	0.42	1.00	605.350	305	74	64	0.65	2.95	101.4
1-02	110.0	0.42	1.00	608.250	301	74	65	0.65	2.90	99.3
1-03	115.0	0.40	0.97	611.070	303	74	65	0.63	2.82	99.1
1-04	120.0	0.47	1.10	614.080	306	73	65	0.69	3.01	97.9
1-05	125.0	0.52	1.30	617.300	307	74	66	0.72	3.22	99.5
Final	125.0		1.23080	78.62000	306.84000	63.80000		0.71221	78.62000	

25 points sampled
QC-Check: Field Averages

Sq. Rt. ΔP	0.7122	1.2308	78.6200	306.8400	63.8000
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Avg. OK
 Avg. OK
 Avg. OK
 Avg. OK
 Avg. OK

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Field Data Printout

Test Method: USEPA Method 29
Analyte: Trace Metals

Location: Unit 3 FF Outlet

Test Run: 3

Client: Wheelabrator North Broward, Inc.

Project No: 10955

Source Area (ft²): 64.00000

Meter Operator: _____
 Probe Operator: _____

Test Date: 12/08/10

Start Time: 13:10

Stop Time: 15:15

Leak Rate Before: 0.003 cfm @ 12 "Hg
 Leak Rate After: 0.001 cfm @ 5 "Hg

Bar. Press. (in. Hg): 30.04

Static P: -10.4

O₂ (dry volume %): 10.13

CO₂ (dry volume %): 8.93

N₂+CO (dry volume %): 80.93

Nozzle ID No: 271-1

Nozzle Diameter (D_n): 0.271

Probe ID No: 67-8-18

Pitot C_p: 0.8200

Pitot Leak Check: Pass Fail

H₂O (condensate, ml or gm): 376.2

H₂O (silica, g): 15.8

Actual Moisture (%): 19.44

Meter Box ID. No: 61-6

Meter ΔH@: 1.76010

Meter Y_d: 0.99600

Traverse Point	Run Time 5.0 min/read	Pitot ΔP _s (in. H ₂ O)	Sample ΔH (in. H ₂ O)	Metered (dcf)	Stack T _s (°F)	Dry Gas Meter		√ΔP _s (calculated) (√in. H ₂ O)	Volume (calculated) (ft ³)	Isokinetics (calculated) (%)
						T _{m-in} (°F)	T _{m-out} (°F)			
	0.0			618.165						
1-01	5.0	0.53	1.30	621.580	306	66	65	0.73	3.42	106.0
1-02	10.0	0.45	1.10	624.540	300	73	67	0.67	2.96	98.4
1-03	15.0	0.35	0.85	627.210	307	75	67	0.59	2.67	100.9
1-04	20.0	0.45	1.10	630.300	307	76	68	0.67	3.09	102.8
1-05	25.0	0.40	0.97	633.120	306	77	68	0.63	2.82	99.3
2-01	30.0	0.60	1.50	636.750	307	79	69	0.77	3.63	104.3
2-02	35.0	0.56	1.40	640.100	309	80	69	0.75	3.35	99.7
2-03	40.0	0.50	1.20	643.200	309	80	70	0.71	3.10	97.5
2-04	45.0	0.45	1.10	646.190	308	80	71	0.67	2.99	98.9
2-05	50.0	0.37	0.90	648.970	307	82	71	0.61	2.78	101.1
3-01	55.0	0.57	1.40	652.420	308	84	72	0.75	3.45	101.0
3-02	60.0	0.50	1.20	655.510	309	86	73	0.71	3.09	96.3
3-03	65.0	0.47	1.10	658.490	310	87	74	0.69	2.98	95.7
3-04	70.0	0.45	1.10	661.450	310	87	75	0.67	2.96	97.1
3-05	75.0	0.45	1.10	664.450	310	87	76	0.67	3.00	98.3
4-01	80.0	0.60	1.50	668.010	310	87	77	0.77	3.56	101.0
4-02	85.0	0.55	1.30	671.290	310	88	78	0.74	3.28	97.0
4-03	90.0	0.53	1.30	674.640	311	88	78	0.73	3.35	101.0
4-04	95.0	0.48	1.20	677.780	311	87	78	0.69	3.14	99.5
4-05	100.0	0.45	1.10	680.880	312	88	79	0.67	3.10	101.3
5-01	105.0	0.48	1.20	683.970	309	89	79	0.69	3.09	97.5
5-02	110.0	0.45	1.10	687.010	314	88	79	0.67	3.04	99.5
5-03	115.0	0.45	1.10	690.030	312	88	79	0.67	3.02	98.7
5-04	120.0	0.45	1.10	693.030	312	89	80	0.67	3.00	97.9
5-05	125.0	0.40	0.97	695.910	311	89	80	0.63	2.88	99.5
Final	125.0		1.16760	77.74500	309.00000	78.44000		0.68951	77.74500	

25 points sampled

Sq.Rt.ΔP

QC-Check: Field Averages

0.6895	1.1676	77.7450	309.0000	78.4400
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Avg. OK Avg. OK Avg. OK Avg. OK Avg. OK

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USEPA Method 4 Laboratory Data

Location: Unit 3 FF Outlet
 Client: Wheelabrator North Broward, Inc.
 Project No: 10955

Test Method: **USEPA Method 29**
 Analyte: **Trace Metals**
 Analyst: C. Slimp
 Analyst Emp No: 558

Test Run: 1

	Contents	Gross (gm)	Tare (gm)	Net (gm)		
Impinger 1	Empty	607.7	415.7	192.0		
Impinger 2	5%HNO3/10%H2O2	685.5	545.3	140.2		
Impinger 3	5%HNO3/10%H2O2	590.9	545.5	45.4		
Impinger 4	Empty	462.8	450.8	12.0		
Impinger 5	4%KMnO4/10%H2SO4	542.6	537.6	5.0		
Impinger 6	4%KMnO4/10%H2SO4	566.7	565.9	0.8	395.4 Liquid (gm)	<i>Field Data Check</i>
Impinger 7	Silica Gel	751.8	730.7	21.1	0.0 less rinse (gm)	
Impinger 8					395.4 Net Liquid (gm)	<input checked="" type="checkbox"/> QA/QC OK
					+ 21.1 Silica Gel (gm)	<input checked="" type="checkbox"/> QA/QC OK
					416.5 Total Vic (gm)	<input checked="" type="checkbox"/> QA/QC OK

Rinse: _____ (ml or gm)

Test Run: 2

	Contents	Gross (gm)	Tare (gm)	Net (gm)		
Impinger 1	Empty	606.4	428.8	177.6		
Impinger 2	5%HNO3/10%H2O2	730.5	621.1	109.4		
Impinger 3	5%HNO3/10%H2O2	589.0	536.3	52.7		
Impinger 4	Empty	478.4	456.1	22.3		
Impinger 5	4%KMnO4/10%H2SO4	554.4	545.8	8.6		
Impinger 6	4%KMnO4/10%H2SO4	540.0	538.1	1.9	372.5 Liquid (gm)	<i>Field Data Check</i>
Impinger 7	Silica Gel	750.6	728.0	22.6	0.0 less rinse (gm)	
Impinger 8					372.5 Net Liquid (gm)	<input checked="" type="checkbox"/> QA/QC OK
					+ 22.6 Silica Gel (gm)	<input checked="" type="checkbox"/> QA/QC OK
					395.1 Total Vic (gm)	<input type="checkbox"/> QA/QC OK

Rinse: _____ (ml or gm)

Test Run: 3

	Contents	Gross (gm)	Tare (gm)	Net (gm)		
Impinger 1	Empty	695.6	419.2	276.4		
Impinger 2	5%HNO3/10%H2O2	629.5	546.7	82.8		
Impinger 3	5%HNO3/10%H2O2	563.3	548.5	14.8		
Impinger 4	Empty	455.3	452.9	2.4		
Impinger 5	4%KMnO4/10%H2SO4	541.9	541.7	0.2		
Impinger 6	4%KMnO4/10%H2SO4	547.9	548.3	-0.4	376.2 Liquid (gm)	<i>Field Data Check</i>
Impinger 7	Silica Gel	767.3	751.5	15.8	0.0 less rinse (gm)	
Impinger 8					376.2 Net Liquid (gm)	<input checked="" type="checkbox"/> QA/QC OK
					+ 15.8 Silica Gel (gm)	<input checked="" type="checkbox"/> QA/QC OK
					392.0 Total Vic (gm)	<input checked="" type="checkbox"/> QA/QC OK

Rinse: _____ (ml or gm)

Test Run: _____

	Contents	Gross (gm)	Tare (gm)	Net (gm)		
Impinger 1	Empty					
Impinger 2	5%HNO3/10%H2O2					
Impinger 3	5%HNO3/10%H2O2					
Impinger 4	Empty					
Impinger 5	4%KMnO4/10%H2SO4					
Impinger 6	4%KMnO4/10%H2SO4				Liquid (gm)	<i>Field Data Check</i>
Impinger 7	Silica Gel				less rinse (gm)	
Impinger 8					Net Liquid (gm)	<input type="checkbox"/> QA/QC OK
					Silica Gel (gm)	<input type="checkbox"/> QA/QC OK
					Total Vic (gm)	<input type="checkbox"/> QA/QC OK

Rinse: _____ (ml or gm)

USEPA Method 3 Laboratory Data

Location: Unit 3 FF Outlet

Client: Wheelabrator North Broward, Inc.

Project No: 10955

Method: EPA Method 3

Fuel Type: Municipal Waste

F_o for Fuel: 1.03 to 1.3

Test Method:

USEPA Method 29

Analyte:

Trace Metals

Analyst: C. Slimp

Analyst Emp No: 558

Run Number	Trial	Percent CO ₂	Percent O ₂ +CO ₂	Percent O ₂	Percent N ₂	Dry Mol. Weight	F _o	Method of Analysis: Orsat
1	1	8.2	19.0	10.8	81.0	29.74	1.22984	All measurements in spec.
	2	8.2	19.0	10.8	81.0	29.74		
	3	8.4	19.0	10.6	81.0	29.77		
Avg.		8.26667		10.73333	81.00000	29.75		
CEM or Other Avg:		<input type="text"/>		<input type="text"/>				<input checked="" type="checkbox"/> Fo value within expected range.

Run Number	Trial	Percent CO ₂	Percent O ₂ +CO ₂	Percent O ₂	Percent N ₂	Dry Mol. Weight	F _o	Method of Analysis: Orsat
2	1	8.2	19.0	10.8	81.0	29.74	1.23984	All measurements in spec.
	2	8.2	19.0	10.8	81.0	29.74		
	3	8.2	18.8	10.6	81.2	29.74		
Avg.		8.20000		10.73333	81.06667	29.74		
CEM or Other Avg:		<input type="text"/>		<input type="text"/>				<input checked="" type="checkbox"/> Fo value within expected range.

Run Number	Trial	Percent CO ₂	Percent O ₂ +CO ₂	Percent O ₂	Percent N ₂	Dry Mol. Weight	F _o	Method of Analysis: Orsat
3	1	9.0	19.2	10.2	80.8	29.85	1.20522	All measurements in spec.
	2	8.8	19.0	10.2	81.0	29.82		
	3	9.0	19.0	10.0	81.0	29.84		
Avg.		8.93333		10.13333	80.93333	29.83		
CEM or Other Avg:		<input type="text"/>		<input type="text"/>				<input checked="" type="checkbox"/> Fo value within expected range.

Run Number	Trial	Percent CO ₂	Percent O ₂ +CO ₂	Percent O ₂	Percent N ₂	Dry Mol. Weight	F _o	Method of Analysis:
	1	<input type="text"/>	<input type="text"/>	<input type="text"/>	<input type="text"/>	<input type="text"/>		
	2	<input type="text"/>	<input type="text"/>	<input type="text"/>	<input type="text"/>	<input type="text"/>		
	3	<input type="text"/>	<input type="text"/>	<input type="text"/>	<input type="text"/>	<input type="text"/>		
Avg.		<input type="text"/>		<input type="text"/>	<input type="text"/>	<input type="text"/>		
CEM or Other Avg:		<input type="text"/>		<input type="text"/>				<input type="checkbox"/> Fo value within expected range.

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WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-7

LABORATORY DATA

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Wheelabrator North Broward, Inc.
 Clean Air Project No: 10955
 Unit 3 FF Outlet

**USEPA Method 29
 Mercury (Hg) Laboratory Parameters**

Blank Analysis

m _{1b-B}	Fraction 1B Blank (µg)	<0.1000
m _{2b-B}	Fraction 2B Blank (µg)	<0.2000
m _{3a-B}	Fraction 3A Blank (µg)	<0.2000
m _{3b-B}	Fraction 3B Blank (µg)	<0.5000
m _{3c-B}	Fraction 3C Blank (µg)	<0.4000
m _{total-B}	Total Blank Amount (µg)	<1.4000

Run No.

	1	2	3
Date (2010)	Dec 8	Dec 8	Dec 8
Start Time (approx.)	08:04	10:45	13:10
Stop Time (approx.)	10:19	12:53	15:15

Sample Analysis

	1	2	3
m _{1b-S}	Fraction 1B Sample (µg)	<0.1000	<0.1000
m _{2b-S}	Fraction 2B Sample (µg)	7.9536	7.4497
m _{3a-S}	Fraction 3A Sample (µg)	<0.2000	0.3763
m _{3b-S}	Fraction 3B Sample (µg)	<0.5000	<0.5000
m _{3c-S}	Fraction 3C Sample (µg)	<0.4000	<0.4000
m _{total-S}	Total Sample Amount (µg)	7.9536	7.8260

Allowable Blank

m _{T-B-allow}	Total Allowable Blank (µg)	0.0000	0.0000	0.0000
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Sample Corrected for Blank

m _n	Total Sample Amount (µg)	7.9536	7.8260	10.7533
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Sample Corrected for Blank

	1	2	3
m _{n-1b}	Fraction 1B (µg)	<0.1000	<0.1000
m _{n-2b}	Fraction 2B (µg)	7.9536	7.4497
m _{n-3a}	Fraction 3A (µg)	<0.2000	0.3763
m _{n-3b}	Fraction 3B (µg)	<0.5000	<0.5000
m _{n-3c}	Fraction 3C (µg)	<0.4000	<0.4000

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Clean Air Engineering, Inc.

500 West Wood Street
Palatine, IL 60067

Project Number: 10955

Mercury

EPA Method 29 Analysis

Analytical Report
15849



Element One, Inc.
5022-C Wrightsville Av., Wilmington, NC 28403
910-793-0128 FAX: 910-792-6853 e1lab@e1lab.com

The following data for Analytical Report 15849
has been reviewed for completeness, accuracy,
adherence to method protocol,
and compliance with quality assurance guidelines.

Review by:



Daphne Woodman, Chemist
December 21, 2010

Report Reviewed and Finalized By:



Ken Smith, Laboratory Director
December 21, 2010

elementOne

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SUMMARY OF RESULTS

elementOne

15849 CAE M29-5 Report Packet
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Summary of Analysis

Summary of Method 29 Mercury Analysis

Run Number		Average Total Catch, μg	Front half μg	H_2O_2 / HNO_3 μg	Empty Impinger μg	KMnO_4 μg	HCl μg
U3 FF Outlet R1	#1	7.95	< 0.1	8.07	< 0.2	< 0.5	< 0.4
	#2		< 0.1	7.83	< 0.2	< 0.5	< 0.4
U3 FF Outlet R2	#1	7.83	< 0.1	7.62	0.389	< 0.5	< 0.4
	#2		< 0.1	7.28	0.363	< 0.5	< 0.4
U3 FF Outlet R3	#1	10.8	< 0.1	11.0	< 0.2	< 0.5	< 0.4
	#2		< 0.1	10.5	< 0.2	< 0.5	< 0.4
Field Blank	#1	< 0.5	< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
	#2		< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
Reagent Blank	#1	< 0.5	< 0.1	< 0.2	< 0.2	< 0.5	< 0.4
	#2		< 0.1	< 0.2	< 0.2	< 0.5	< 0.4

ANALYTICAL NARRATIVE

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Element One Analytical Narrative

Client:	Clean Air, IL	Element One #:	15849
Client ID:	10955/N. Broward	Analyst:	DV & VA
Method:	Methods 29	Dates Received:	12/09/10
Analytes:	Hg	Dates Analyzed:	12/10-20/10

Summary of Analysis

The Method 29 samples were digested, prepared, and analyzed according to Method 29 protocol. Samples were analyzed for mercury on a PerkinElmer FIMS-100 CVAA mercury analyzer.

Detection Limits

The FIMS-100 CVAA instrument reporting limit for mercury was 0.004 µg per aliquot analyzed.

Analysis QA/QC

Duplicate analyses relative percent difference (RPD) and spike sample recovery data are summarized in the Quality Control Section. All QA/QC data was within the criteria of the method.

Additional Comments

The reported results have not been corrected for any blank values or spike recovery values.

QUALITY CONTROL SUMMARY

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Summary of Quality Control Data

Mercury Duplicate Analysis RPD

(Method 29 QC limits: < 10% for RPD)

Run Number	Front half	H ₂ O ₂ /HNO ₃	Empty Imp	KMnO ₄	HCl
U3 FF Outlet R1	NA	3.0%	NA	NA	NA
U3 FF Outlet R2	NA	4.5%	7.0%	NA	NA
U3 FF Outlet R3	NA	4.8%	NA	NA	NA
Field Blank	NA	NA	NA	NA	NA
Reagent Blank	NA	NA	NA	NA	NA

Mercury Spike Recoveries

(Method 29 QC limits: ± 25% for Spike Recoveries)

Run Number		Front half	H ₂ O ₂ /HNO ₄	Empty Imp	KMnO ₄	HCl
U3 FF Outlet R3	#1	115%	106%	117%	112%	105%
	#2	113%	110%	109%	113%	94%

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SAMPLE CUSTODY

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CHAIN OF CUSTODY FORM

15849 201623

CLIENT <u>Wheelerator</u>		PROJECT NO. <u>10955</u>		NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED				PAGE <u>1</u> OF <u>3</u>
PLANT <u>N. Broward</u>		DEPT. <u>66</u>				/ / / / /				REVISION NO. <u>1</u>
PROJECT MANAGER <u>S. Brown</u>		RECOVERY PERSON: <u>C. Slomp</u>								ADDITIONAL INFORMATION
JOB LEADER <u>C. Slomp</u>										
CAE LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX						
	Blank	Lab	12/8	Quartz Filter Blank	1	N/A	✓			
	Field Blank	Unit 3 FF Outlet	12/8	Quartz Filter - Field Quartz	1	"	✓			
	1	"	12/8	Quartz Filter	1	"	✓			
	2	"	12/8	"	1	"	✓			
	3	"	12/8	"	1	"	✓			
	Blank	Lab	12/8	8V HCl Rinse of Imp 506	1	225	✓			
	Field Blank	Unit 3 FF Outlets	12/8	"		225	✓			
	1	"	12/8	"		225	✓			
	2	"	12/8	"		225	✓			
	3	"	12/8	"		225	✓			
	Repeat Blank	Lab	12/8	DI water	1	100	✓			
Relinquished by:(Signature)		Date/Time	Received by:(Signature)		Date/Time	Relinquished by:(Signature)		Date/Time		
<u>Carl Slomp</u>		12/8/10	<u>Carl Slomp</u>			<u>Anna Brown</u>		12/9/10 1010		
Courier:		Date/Time	Relinquished by:(Signature)		Date/Time	Rec'd for Analysis by:		Date/Time		
						<u>Anna Brown</u>				
Special Handling Instructions <u>Attn: Ken Smith</u>			This form was completed by:			Samples received in good condition in fisherbrand containers. No empty containers received.				
Forwarding Lab: <u>Element One</u>			<u>Carl Slomp</u>			Clean Air Engineering				
<u>5022-C Wrightville Ave</u>			Signature			500 West Wood Street				
<u>Wilmington, NC 28405</u>			Date			Palatine, IL 60067				
PO Number:			<u>Carl Slomp 12/8/10</u>			800-627-0033 Fax (847) 991-3385				

CHAIN OF CUSTODY FORM

15849

201487

CLIENT <u>Wheelerator</u>		PROJECT NO. <u>10955</u>		NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED				PAGE <u>2</u> OF <u>3</u>
PLANT <u>N. Browns</u>		DEPT. <u>66</u>				/ / / / /				REVISION NO. <u>1</u>
PROJECT MANAGER <u>G. Brown</u>		RECOVERY PERSON: <u>Carl Slings</u>								ADDITIONAL INFORMATION
JOB LEADER <u>C. Slings</u>										
CAE LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX						
	Blank	Lab	12/8/10	51. HNO ₃ / 10x H ₂ O dist	1	200	✓			
	Field Blank	FF Outlet U3	"	Temp 3 catch + rinse	1	300	✓			
	1	"	"	"	1	667	✓			
	2	"	"	"	1	614	✓			
	3	"	"	"	1	423	✓			
	Blank	Lab	12/8/10	0.1N HNO ₃	1	100	✓			
	Field Blank	FF Outlet	"	Temp 4 catch + rinse	1	100	✓			
	1	"	"	"	1	110	✓			
	2	"	"	"	1	117	✓			
	3	"	"	"	1	108	✓			
Relinquished by: (Signature)		Date/Time	Received by: (Signature)		Date/Time	Relinquished by: (Signature)		Date/Time		
<u>Carl Slings</u>		12/8/10	<u>Carl Slings</u>							
Courier:		Date/Time	Relinquished by: (Signature)		Date/Time	Rec'd for Analysis by:		Date/Time		
						<u>Dina Braten</u>		12/9/10 1010		
Special Handling Instructions <u>Attn: Ken Smith</u>			This form was completed by:			Clean Air Engineering 500 West Wood Street Palatine, IL 60067 800-627-0033 Fax (847) 991-3385 <small>DS COC Palatine EXCL.FD-6/7/98</small>				
Forwarding Lab: <u>Element One</u>			<u>Carl Slings</u>							
<u>5022-C Wrightsville Ave</u>			Signature	Date						
<u>Wilmington, NC 28405</u>			<u>Carl Slings</u>	12/8/10						
PO Number:										

CHAIN OF CUSTODY FORM

15849

201486

CLIENT <u>Wheelabrator</u>		PROJECT NO. <u>10955</u>		NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED			PAGE <u>3</u> OF <u>3</u>
PLANT <u>North Downs</u>		DEPT. <u>66</u>				/ / / / / / / / / /			REVISION NO. <u>1</u>
PROJECT MANAGER <u>Scott Brown</u>		RECOVERY PERSON: <u>Carl Slimp</u>							ADDITIONAL INFORMATION
JOB LEADER <u>Carl Slimp</u>									
CAE LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX					
	Blank	Lab	12/8	4% KMnO ₄ /10% H ₂ SO ₄ Blank	1	100	✓		
	Field Obs	FF Outlet U3	12/4/10	Imp Catch #5 + 6	1	400	✓		
	1	"	"	Imp #5 + 6 Catch + Rinse	1	420	✓		
	2	"	"	"	1	420	✓		
	3	"	"	"	1	563			
	Field Obs	FF Outlet U3	12/8/10	F 1/2 Rinse Oil Mbric	1	100	✓		
	1		"		1	100	✓		
	2		"		1	100	✓		
	3		"		1	100	✓		
Relinquished by: (Signature)		Date/Time	Received by: (Signature)		Date/Time	Relinquished by: (Signature)		Date/Time	
<u>Carl Slimp</u>		12/8	<u>Carl Slimp</u>						
Courier:		Date/Time	Relinquished by: (Signature)		Date/Time	Rec'd for Analysis by:		Date/Time	
						<u>Scott Brown</u>		12/9/10 1010	
Special Handling Instructions <u>Attn: Ken Smith</u>			This form was completed by:			Clean Air Engineering 500 West Wood Street Palatine, IL 60067 800-627-0033 Fax (847) 991-3385			
Forwarding Lab: <u>Element One</u>			<u>Carl Slimp</u>						
<u>5022-C Wrightsville Ave</u>			Signature Date						
<u>Wilmington, NC 28405</u>			<u>Carl Slimp</u> 12/8/10			03 OGC Palatine EXCL 90-07/08			
PO Number:									

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ANALYTICAL DATA

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Analytical Calculations

Mercury-

$$\text{Mercury Results } (\mu\text{g}) = \frac{\text{CVAA Results } (\mu\text{g}) * \text{Final Volume (ml)}}{\text{Aliquot (ml)}}$$

Where-

CVAA Results= Raw sample reading (μg)--*Hg-Data Sheet*

Aliquot= Sample Aliquot (Alq.)--*Hg-Data Sheet*

Final Volume=Final Volume (FV)*--*Sample Submission*

* With the exception of the BH fraction where-
=Received Volume (BV)--*Sample Submission*

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Analytical Calculations

Spike Recovery-

$$\text{Spike (\%)} = \frac{(\text{Spiked Result } (\mu\text{g/L}) - \text{Sample Result } (\mu\text{g/L}))}{\text{Spike Amount } (\mu\text{g/L})} \times 100$$

Where-

Spike Result = Raw sample concentration (ppb)--*ICP-Data Sheet*

Sample Result = Raw sample concentration (ppb)--*ICP-Data Sheet*

Spike Amount--*ICP-MS Spike Table*

Duplicate Analysis RPD-

$$\text{RPD (\%)} = \frac{(\text{Duplicate Result } (\mu\text{g/L}) - \text{Sample Result } (\mu\text{g/L}))}{\text{Average } (\mu\text{g/L})} \times 100$$

Where-

Sample Result and Duplicate Results=Raw sample concentration (ppb)--*ICP-Data Sheet*

$$\text{Average} = \frac{(\text{Duplicate} + \text{Sample Results})}{2}$$

elementOne AIR TESTING SAMPLE SUBMISSION FORM Lab ID 15849



Analysis Due Date 12.16.10
QA/QC/Report Due Date 12.20.10

Client Clean Air IL
Project No 10955

Date Rec 12.09.10
Time Rec 1010

HNO₃ Lot: 1110060 HF Lot: 5109120 HCl Lot: 4110060
Volume Marked N Volume Loss Y/ N? Ref. Method: 29

Sample Identification

1	U3 FF Outlet R1	4	Field Blank
2	U3 FF Outlet R2	5	Reagent Blank
	U3 FF Outlet R2 Duplicate		
3	U3 FF Outlet R3		
	U3 FF Outlet R3 Spike		

Analyses Requested

Samples 1-5 Hg

Runs / FB	Fil / Ace (FH)		HNO ₃ (FH)		5% HNO ₃ /10% H ₂ O ₂ (BH)			HNO ₃ (A)		KMnO ₄ (B)		HCl (C)	
	pH <2.0	Y/N	pH <2.0	Y/N	BV ml	Used	FV ml	pH <2.0	Y/N	pH <2.0	Y/N	pH <2.0	Y/N
Lab ID	Fil ID	BV ml	BV ml	FV ml	BV ml		FV ml	BV ml	FV ml	BV ml	FV ml	BV ml	FV ml
1			100	100	660			114	200	390	500	280	400
2.D			100		650			116		370		230	
3.S			100		660			106		370		230	
4			100		290			102		280		230	

M-29 Reagent Blank

Lab ID	Fraction	BV, ml	FV, ml	Comments
5	C-7 FH Acetone Blank			* 90 mL C10 was combined
	C-8A FH 0.1N HNO ₃	300		with 30 mL C8B for
	C-8A A 0.1N HNO ₃			B Fraction for a final
	C-8B B DI H ₂ O	100		volume of 120ml
	C-9 BH 5% HNO ₃ /10% H ₂ O ₂	190		
	C-10 B 4% KMnO ₄ /10% H ₂ SO ₄	90		* used 100 mL C8A for
	C-11 C 8N HCl DI H ₂ O	230	400	Front half
	C-12 FH Filter			

Lab Communications

FH spiked w/ 200 µL Standard A

Fractions Received c1, c3, c4, c5a, c5b, c5c; c12, c8a, c8b, c9, c10, c11—LLB 12.09.10

SS Page 1 of 1
12/10/2010 9:04:13 AM
SS by ZJB
Labeled By/Date ZJB 12/10/10

FH Prep By/Date VA 12.13.10 A Prep By/Date VA 12.10.10
BH Prep By/Date ↓ B Prep By/Date ↓
BH/FH Prep By/Date ↓ C Prep By/Date VA 12.13.10
PM Prep By/Date ↓ ID Verification By/Date VA 12.10.10

PerkinElmer FIMS-100 CVAA Mercury Analyzer

Sample_ID	Date	Time	Mean_Sig	Mean_Rd	Mean_Rt	Units	Alq.	Vol.	Sig 1	Reading-1	Result-1	Sig 2	Reading-2	Result-2
STD2=.04ug	12/14/2010	16:32:16	0.0086581			µg	0.4	600	0.0086581					
STD3=.08ug	12/14/2010	16:33:33	0.0178971			µg	0.4	600	0.0178971					
STD4=.16ug	12/14/2010	16:34:49	0.0370032			µg	0.4	600	0.0370032					
STD5=.2ug	12/14/2010	16:36:07	0.0437011			µg	0.4	600	0.0437011					
Reagent Blank	12/14/2010	16:37:53	9.942E-05	0.0004448	0.0004448	µg	0.4	600	0.000134	0.0005993	0.0005993	6.488E-05	0.0002903	0.0002903
0.004ug = DL	12/14/2010	16:41:32	0.0009244	0.0041354	0.0041354	µg	0.4	600	0.0009244	0.0041354	0.0041354			
0.080ug = STD.2	12/14/2010	16:45:19	0.0187923	0.0840704	0.0840704	µg	0.4	600	0.0187923	0.0840704	0.0840704			
REAGENT BLANK	12/14/2010	16:46:35	0.0001596	0.0007141	0.0007141	µg	0.4	600	0.0001596	0.0007141	0.0007141			
15849 FH LRB	12/14/2010	16:48:19	3.738E-05	0.0001672	0.0041807	µg	4	100	2.631E-05	0.0001177	0.0029428	4.844E-05	0.0002167	0.0054186
15849 FH LRB spk	12/14/2010	16:50:03	0.0168969	0.075591	4.7244395	µg	1.6	100	0.0171099	0.0765441	4.7840051	0.0166838	0.074638	4.664874
15849-2 BH	12/14/2010	16:51:48	0.0102476	0.0458442	7.4496796	µg	4	650	0.0104785	0.0468772	7.6175446	0.0100167	0.0448112	7.2818146
15849-2 BH dup	12/14/2010	16:53:34	0.0094529	0.0422892	6.8719911	µg	4	650	0.0097189	0.043479	7.0853364	0.009187	0.0410994	6.6786459
0.004ug = DL	12/14/2010	17:06:57	0.0008647	0.0038683	0.0038683	µg	0.4	600	0.0008647	0.0038683	0.0038683			
0.080ug = STD.2	12/14/2010	17:08:12	0.0177241	0.0792917	0.0792917	µg	0.4	600	0.0177241	0.0792917	0.0792917			
REAGENT BLANK	12/14/2010	17:09:28	0.0003261	0.0014589	0.0014589	µg	0.4	600	0.0003261	0.0014589	0.0014589			
15849-1 BH	12/14/2010	17:14:40	0.010775	0.0482036	7.9535941	µg	4	660	0.010937	0.0489283	8.0731772	0.010613	0.0474789	7.834011
0.004ug = DL	12/14/2010	17:15:54	0.00095	0.0042502	0.0042502	µg	4	660	0.00095	0.0042502	0.0042502			
0.080ug = QC STD 3	12/14/2010	17:17:11	0.0166195	0.0743502	0.0743502	µg	4	660	0.0166195	0.0743502	0.0743502			
REAGENT BLANK	12/14/2010	17:18:27	0.0003336	0.0014925	0.0014925	µg	4	660	0.0003336	0.0014925	0.0014925			
Calib Blank	12/15/2010	12:29:11	0.0001099			µg			0.0001099					
STD1=.004ug	12/15/2010	12:30:25	0.0008975			µg			0.0008975					
STD2=.04ug	12/15/2010	12:31:40	0.0064427			µg			0.0064427					
STD3=.08ug	12/15/2010	12:32:56	0.01313			µg			0.01313					
STD4=.16ug	12/15/2010	12:34:12	0.0302799			µg			0.0302799					
STD5=.2ug	12/15/2010	12:35:30	0.030119			µg			0.030119					
0.004ug = DL	12/15/2010	12:38:31	0.0007048	0.0038347	0.0038347	µg			0.0007048	0.0038347	0.0038347			
0.080ug = STD.2	12/15/2010	12:41:07	0.0159773	0.0869259	0.0869259	µg			0.0159773	0.0869259	0.0869259			
0.080ug = QC STD 3	12/15/2010	12:42:51	0.0160657	0.0874069	0.0874069	µg			0.0160657	0.0874069	0.0874069			
15849-1 C	12/15/2010	12:45:50	0.0003047	0.0016576	0.1657626	µg	4	400	0.000342	0.0018606	0.1860557	0.0002674	0.0014547	0.1454695
15849-2 C	12/15/2010	12:47:35	0.0005429	0.0029534	0.2953447	µg	4	400	0.0006373	0.0034673	0.34673	0.0004484	0.0024396	0.2439594
15849-2 C dup	12/15/2010	12:49:21	0.0006247	0.0033985	0.3398479	µg	4	400	0.0006608	0.0035952	0.3595166	0.0005885	0.0032018	0.3201791
15849-3 C	12/15/2010	12:51:06	0.000194	0.0010553	0.1055292	µg	4	400	0.0002321	0.0012628	0.1262813	0.0001558	0.0008478	0.0847772
15849-3 C spk	12/15/2010	12:52:54	0.0146358	0.0796276	7.9627603	µg	4	400	0.0154149	0.0838665	8.386648	0.0138567	0.0753887	7.5388726
15849-5 C	12/15/2010	12:56:31	0.0001916	0.0010424	0.1042371	µg	4	400	0.00021	0.0011424	0.1142388	0.0001732	0.0009424	0.0942355
0.004ug = DL	12/15/2010	13:05:28	0.0007909	0.0043032	0.0043032	µg	4	400	0.0007909	0.0043032	0.0043032			
0.080ug = STD.2	12/15/2010	13:08:03	0.0153823	0.0836887	0.0836887	µg	4	400	0.0153823	0.0836887	0.0836887			
REAGENT BLANK	12/15/2010	13:09:19	0.0001592	0.0008659	0.0008659	µg	4	400	0.0001592	0.0008659	0.0008659			
Calib Blank	12/20/2010	13:03:20	0.0004034			µg			0.0004034					
STD1=.004ug	12/20/2010	13:04:35	0.0009064			µg			0.0009064					
STD2=.04ug	12/20/2010	13:05:52	0.0098448			µg			0.0098448					
STD3=.08ug	12/20/2010	13:07:09	0.0208179			µg			0.0208179					
STD4=.16ug	12/20/2010	13:08:27	0.0404666			µg			0.0404666					
STD5=.2ug	12/20/2010	13:09:47	0.0499321			µg			0.0499321					
Reagent Blank	12/20/2010	13:11:35	-0.0000337	-0.0001341	-0.0001341	µg			-0.0000091	-0.0000362	-0.0000362	-0.0000584	-0.000232	-0.000232
0.004ug = DL	12/20/2010	13:12:49	0.0009315	0.0037015	0.0037015	µg			0.0009315	0.0037015	0.0037015			
0.080ug = STD.2	12/20/2010	13:15:26	0.0210747	0.0837398	0.0837398	µg			0.0210747	0.0837398	0.0837398			
0.080ug = QC STD 3	12/20/2010	13:20:40	0.0211719	0.0841261	0.0841261	µg			0.0211719	0.0841261	0.0841261			
REAGENT BLANK	12/20/2010	13:21:57	0.0001216	0.0004831	0.0004831	µg			0.0001216	0.0004831	0.0004831			
15849-4 C	12/20/2010	13:23:43	0.0001144	0.0004544	0.0454369	µg	4	400	8.326E-05	0.0003308	0.0330847	0.0001454	0.0005779	0.0577892
0.004ug = DL	12/20/2010	13:43:36	0.0009652	0.0038351	0.0038351	µg	4	100	0.0009652	0.0038351	0.0038351			
0.080ug = STD.2	12/20/2010	13:44:53	0.0217067	0.0862512	0.0862512	µg	4	100	0.0217067	0.0862512	0.0862512			
REAGENT BLANK	12/20/2010	13:46:10	0.000152	0.0006038	0.0006038	µg	4	100	0.000152	0.0006038	0.0006038			

WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-7

PLANT DATA

H

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**WHEELABRATOR NORTH BROWARD
TONS OF REFUSE PROCESSED PER STACK TEST RUN LOG**

UNIT #3						
Date	Test	Method #	Run #	Steam (klb/hr)	Run Length (hr)	Trash Processed (tons)
12/8/2010	Mercury	29	1	179.6	2.25	65.6
12/8/2010	Mercury	29	2	179.9	2.13	62.2
12/8/2010	Mercury	29	3	180.0	2.08	60.8

**Wheelabrator
NORTH BROWARD
Emission Test Log**

Date: 12/08/10
Start Time: 8:04:00
End Time: 10:19:00

	SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FLOW	DILUTE WATER FLOW	TOTAL LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS	SPECIFIC GRAVITY	
	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O	" H2O
Unit 1	510.10	319.64	37.68	27.04	10.64	15.85	304.10	7.18	-10.64	1.101
Unit 2	511.79	319.76	36.33	26.55	9.78	16.54	293.74	6.49	-10.19	1.101
Unit 3	506.53	320.05	37.76	27.52	10.24	16.43	306.35	6.50	-8.03	1.101

H - 4

	FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNCR CHEM FLOW	STEAM FLOW	AVAILABLE CaO
	KLBS/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBS/hr	
Unit 1	188.23	895.89	825.59	68.97	-0.10	260.67	1212.91	2.50	180.27	1.056
Unit 2	186.93	898.09	827.02	80.19	-0.10	271.96	1270.85	2.79	180.52	1.056
Unit 3	189.39	900.07	833.23	76.59	-0.09	280.93	1162.43	3.34	179.62	1.056

U1 lime (#/hr) 673.89 8.09
U2 lime (#/hr) 619.48 7.43
U3 lime (#/hr) 648.70 7.78

**Wheelabrator
NORTH BROWARD
Emission Test Log**

Date: 12/08/10
Start Time: 10:45:00
End Time: 12:53:00

	SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF/OUT TEMP	FF DP	ID INLET PRESS	SPECIFIC GRAVITY
	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O	" H2O
Unit 1	514.62	320.23	39.65	29.35	10.30	15.32	304.67	7.32	-10.96	1.099
Unit 2	511.69	319.84	35.94	29.61	6.33	16.97	292.87	6.29	-9.84	1.099
Unit 3	509.19	319.85	38.14	30.36	7.78	17.03	306.82	6.44	-7.77	1.099

	FEED H2O FLOW	SH/OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	EGONO OUT TEMP	SH ROLL AVG	SNCR CHEM FLOW	STEAM FLOW	AVAILABLE CaO
	KLBs/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBs/hr	
Unit 1	187.22	895.58	824.02	70.29	-0.10	260.94	1236.56	2.51	179.91	1.039
Unit 2	186.86	897.89	830.97	80.68	-0.10	271.90	1270.43	2.49	179.73	1.039
Unit 3	189.04	899.62	826.82	77.60	-0.09	280.84	1157.99	3.00	179.93	1.039

U1 lime (#/hr) 642.26 7.71
U2 lime (#/hr) 394.51 4.73
U3 lime (#/hr) 484.88 5.82

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**Wheelabrator
NORTH BROWARD
Emission Test Log**

Date: 12/08/10
Start Time: 13:10:00
End Time: 15:15:00

	SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FLOW	WDL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS	SPECIFIC GRAVITY
	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O	" H2O
Unit 1	520.38	319.73	42.45	34.12	8.33	14.72	304.03	7.36	-11.22	1.098
Unit 2	520.97	320.25	39.63	33.18	6.45	15.78	294.06	6.46	-10.17	1.098
Unit 3	511.37	320.22	39.12	29.23	9.89	17.04	307.83	6.50	-7.70	1.098

End of Appendix
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	FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNGR CHEM FLOW	STEAM FLOW	AVAILABLE CaO
	KLBs/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBs/hr	
Unit 1	187.88	895.51	824.35	70.39	-0.10	261.42	1238.55	2.50	180.21	1.024
Unit 2	186.19	897.62	828.30	80.81	-0.10	272.04	1266.14	2.54	179.97	1.024
Unit 3	188.83	899.48	826.08	77.37	-0.09	280.98	1162.28	3.47	180.02	1.024

U1 lime (#/hr)	511.76	6.14
U2 lime (#/hr)	396.05	4.75
U3 lime (#/hr)	607.70	7.29