



Wheelabrator North Broward Inc.

A Waste Management Company

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RECEIVED

JUL 06 2010

**BUREAU OF
AIR REGULATION**

June 28, 2010

CERTIFIED MAIL #70080500000147115632

Mr. Lennon Anderson
Air Program Administrator
Florida Department of Environmental Protection
Southeast District
400 North Congress Ave., Suite 200
West Palm Beach, FL 33401

Re: Wheelabrator North Broward
F.A.C. 62-296.416 Quarterly Mercury Stack Testing
Second Quarter of 2010, Report Submittal

Dear Mr. Anderson:

As required by F.A.C. 62-296.416, please find enclosed the 2010 second quarter report on mercury stack testing which was conducted on Unit #2.

I, the undersigned, am a responsible official, as defined in Rule 62-210.200, F.A.C., of the Title V source addressed in this submittal. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements and information in this document are true, accurate and complete.

If there are any questions, please contact this office at (954) 971-8701.

Sincerely,

Scott McIlvaine
Plant Manager

cc: USEPA, Region IV, Pesticides and Toxics Management Division, Air & EPCRA Enforcement
Branch, Air Enforcement Section CERTIFIED MAIL #70080500000147115649
FDEP, Tallahassee, Bureau of Air Regulation, New Source Review Section,
CERTIFIED MAIL #70080500000147115656
Broward County Department of Planning and Environmental Protection, Air Quality Division
CERTIFIED MAIL #70080500000147115663

Chuck Faller (with)
Tim Porter (without)
Rob French - MPI - (with)
Ram Tewari - BCWRS (without)

REPORT ON MERCURY TESTING

**WHEELABRATOR NORTH BROWARD, INC.
UNIT 2 FF OUTLET
POMPANO BEACH, FL**

**CLEANAIR PROJECT NO: 10955-5
REVISION 0: JUNE 21, 2010**

CleanAir.

Scott Brown
Project Manager

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CleanAir Engineering
500 W. Wood Street
Palatine, IL 60067-4975





Wheelabrator North Broward, Inc.
2600 NW 48th Street
Pompano Beach, FL 33073

REPORT ON MERCURY TESTING

Performed for:
WHEELABRATOR NORTH BROWARD, INC.
UNIT 2 FF OUTLET
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-5
Revision 0: June 21, 2010

To the best of our knowledge, the data presented in this report are accurate, complete, error free, legible and representative of the actual emissions during the test program.

Submitted by,

A handwritten signature in black ink, appearing to read "Scott Brown".

Scott Brown
Project Manager
sbrown@cleanair.com
(800) 627-0033

Reviewed by,

A handwritten signature in black ink, appearing to read "Kevin O'Halloren".

Kevin O'Halloren, PE
Project Manager
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WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-5

REVISION HISTORY

ii

REPORT ON MERCURY TESTING

DRAFT REPORT REVISION HISTORY

Revision:	Date	Pages	Comments
D0a	06/15/10	All	Draft version of original document.

FINAL REPORT REVISION HISTORY

Revision:	Date	Pages	Comments
0	06/21/10	All	Final version of original document.

CONTENTS

1 PROJECT OVERVIEW 1-1
 Table 1-1: Schedule of Activities 1-1
 Table 1-2: Summary of Test Results 1-2

2 RESULTS 2-1
 Table 2-1: Unit 2 FF Outlet – Mercury 2-1
 Table 2-2: Quality Assurance and Quality Control 2-2

3 DESCRIPTION OF INSTALLATION 3-1
 PROCESS DESCRIPTION 3-1
 Figure 3-1: General Process Schematic 3-1
 Figure 3-2: Process Schematic 3-2
 DESCRIPTION OF SAMPLING LOCATION(S) 3-3
 Table 3-1: Sampling Points 3-3
 Figure 3-3: Unit 2 FF Outlet Sampling Point Determination (EPA Method 1) 3-3

4 METHODOLOGY 4-1
 Table 4-1: Summary of Sampling Procedures 4-1

5 APPENDIX 5-1
 TEST METHOD SPECIFICATIONS A
 SAMPLE CALCULATIONS B
 PARAMETERS C
 QA/QC DATA D
 FIELD DATA E
 FIELD DATA PRINTOUTS F
 LABORATORY DATA G
 PLANT DATA H

WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-5

PROJECT OVERVIEW

1-1

Wheelabrator North Broward, Inc. operates a refuse to energy facility, located in Pompano Beach, Florida. The facility's emission levels are regulated by the Florida Department of Environmental Protection (FDEP). Wheelabrator North Broward, Inc. contracted Clean Air Engineering (CleanAir) to perform a compliance test program at its municipal waste combustor (MWC) facility in Pompano Beach, Florida. Testing was conducted in accordance with 40 CFR 60 Subpart Cb and applicable sections of PSD-FL-112(B) and PA86-22. The sampling was conducted at the Unit 2 Fabric Filter (FF) Outlet on May 25, 2010.

The testing included the determination of the following constituents:

- moisture (H₂O);
- oxygen (O₂);
- carbon dioxide (CO₂);
- total flow (dscfm);
- mercury (Hg).

Coordinating and observing the field portion of the program were:

C. Faller	- Wheelabrator North Broward, Inc.
C. Slimp	- CleanAir
P. Bihun	- CleanAir

Chuck Faller of Wheelabrator North Broward Inc. provided all the process (operating) data. This data is presented in its entirety in Appendix H.

All equipment utilized for testing was manufactured by Clean Air Engineering.

Table 1-1 outlines the schedule adhered to during the test program. Table 1-2 (on page 1-2) summarizes the results of the test program.

**Table 1-1:
Schedule of Activities**

Run Number	Location	Method	Analyte	Date	Start Time	End Time
1	Unit 2 FF Outlet	USEPA Method 29	Mercury	05/25/10	07:39	09:50
2	Unit 2 FF Outlet	USEPA Method 29	Mercury	05/25/10	10:18	12:29
3	Unit 2 FF Outlet	USEPA Method 29	Mercury	05/25/10	12:50	15:00

PROJECT OVERVIEW

1-2

**Table 1-2:
Summary of Test Results**

<u>Source</u> Constituent	Sampling Method	Average Emission	Permit Limit ¹
Unit 2 FF Outlet Mercury ($\mu\text{g}/\text{dscm}$ @7% O ₂)	EPA M29	15	50

¹ Limit obtained from the facility's Title V Permit No. 0570127-005-AV and Subpart Cb as of April 28, 2009

The test conditions and results of analysis are presented in Table 2-1 (on page 2-1) and the quality control and quality assurance results are shown in Table 2-2 (on page 2-2).

End of Section 1 – Project Overview

WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-5

RESULTS

2-1

**Table 2-1:
Unit 2 FF Outlet – Mercury**

Run No.	1	2	3	Average
Date (2010)	May 25	May 25	May 25	
Start Time (approx.)	07:39	10:18	12:50	
Stop Time (approx.)	09:50	12:29	15:00	
Process Conditions				
R _p Steam Production Rate (Klbs/hour)	185	184	184	184
P ₁ SDA Outlet Temperature (°F)	319	320	320	320
Gas Conditions				
O ₂ Oxygen (dry volume %)	9.0	9.0	9.0	9.0
CO ₂ Carbon dioxide (dry volume %)	9.6	9.8	9.8	9.7
T _s Sample temperature (°F)	309	309	309	309
B _w Actual water vapor in gas (% by volume)	23.9	23.5	23.9	23.7
Gas Flow Rate				
Q _a Volumetric flow rate, actual (acfm)	183,571	174,827	179,796	179,398
Q _{std} Volumetric flow rate, dry standard (dscfm)	93,659	89,469	91,496	91,542
Sampling Data				
V _{mstd} Volume metered, standard (dscf)	77.82	72.71	74.05	74.86
%I Isokinetic sampling (%)	104.7	102.4	102.0	103.0
Laboratory Data				
m _{n-1b} Fraction 1B (µg)	0.1204	<0.1000	<0.1000	
m _{n-2b} Fraction 2B (µg)	42.0524	20.5021	19.5846	
m _{n-3a} Fraction 3A (µg)	<0.2000	<0.2000	<0.2000	
m _{n-3b} Fraction 3B (µg)	<0.5000	<0.5000	<0.5000	
m _{n-3c} Fraction 3C (µg)	0.8843	<0.4000	<0.4000	
m _n Total matter corrected for allowable blanks (µg)	43.0571	20.5021	19.5846	
Mercury Results - Total				
C _{sd} Concentration (lb/dscf)	1.2E-09	6.2E-10	5.8E-10	8.1E-10
C _{sd7} Concentration @7% O ₂ (lb/dscf)	1.4E-09	7.3E-10	6.8E-10	9.5E-10
C _{sd} Concentration (µg/dscm)	20	10	9	13
C _{sd7} Concentration @7% O ₂ (µg/dscm)	23	12	11	15
E _{lb/hr} Rate (lb/hr)	0.0069	0.0033	0.0032	0.0045
E _{Fd} Rate - Fd-based (lb/MMBtu)	2.1E-05	1.0E-05	9.8E-06	1.4E-05

RESULTS

2-2

**Table 2-2:
Quality Assurance and Quality Control**

RPD RESULTS						
Run Number	Front Half	H ₂ O ₂ /HNO ₄	Empty Impinger	KMnO ₄	HCl	
U2 FF Outlet R1	0.034	0.006	NA	NA	0.011	
U2 FF Outlet R2	NA	0.00099678	NA	NA	NA	
U2 FF Outlet R3	NA	0.006	NA	NA	NA	
Field Blank	NA	NA	NA	NA	NA	
Reagent Blank	NA	NA	NA	NA	NA	
Sample Spike and Recovery						
U2 FF Outlet R3	#1 98%	102%	82%	92%	115%	
	#2 108%	105%	83%	91%	113%	
Blanks						
Field Blank	#1 < 0.1	< 0.3	< 0.2	< 0.5	< 0.4	
	#2 < 0.1	< 0.3	< 0.2	< 0.5	< 0.4	
Reagent Blank	#1 < 0.1	< 0.2	< 0.2	< 0.5	< 0.4	
	#2 < 0.1	< 0.2	< 0.2	< 0.5	< 0.4	
Meter Post Cal	-0.6%					

End of Section 2 – Results

DESCRIPTION OF INSTALLATION

3-1

PROCESS DESCRIPTION

The North Broward Resource Recovery Facility operates three (3) 750 tons per day municipal refuse-fired, water-wall boiler trains. The trains were manufactured by Babcock & Wilcox to produce electricity for sale to a local utility company. Each boiler is equipped with a spray dryer absorber (SDA) for acid gas removal, followed by a fabric filter (FF) baghouse for the control of particulate emissions. Wheelabrator Air Pollution Control, Inc. supplies the control equipment. Each FF baghouse is followed by an induced draft fan that directs the flue gas to a dedicated flue in a common stack.

Figure 3-1 shows a general schematic for the facility. The testing occurred at the Unit 2 FF Outlet as shown in Figure 3-2 (on page 3-2).

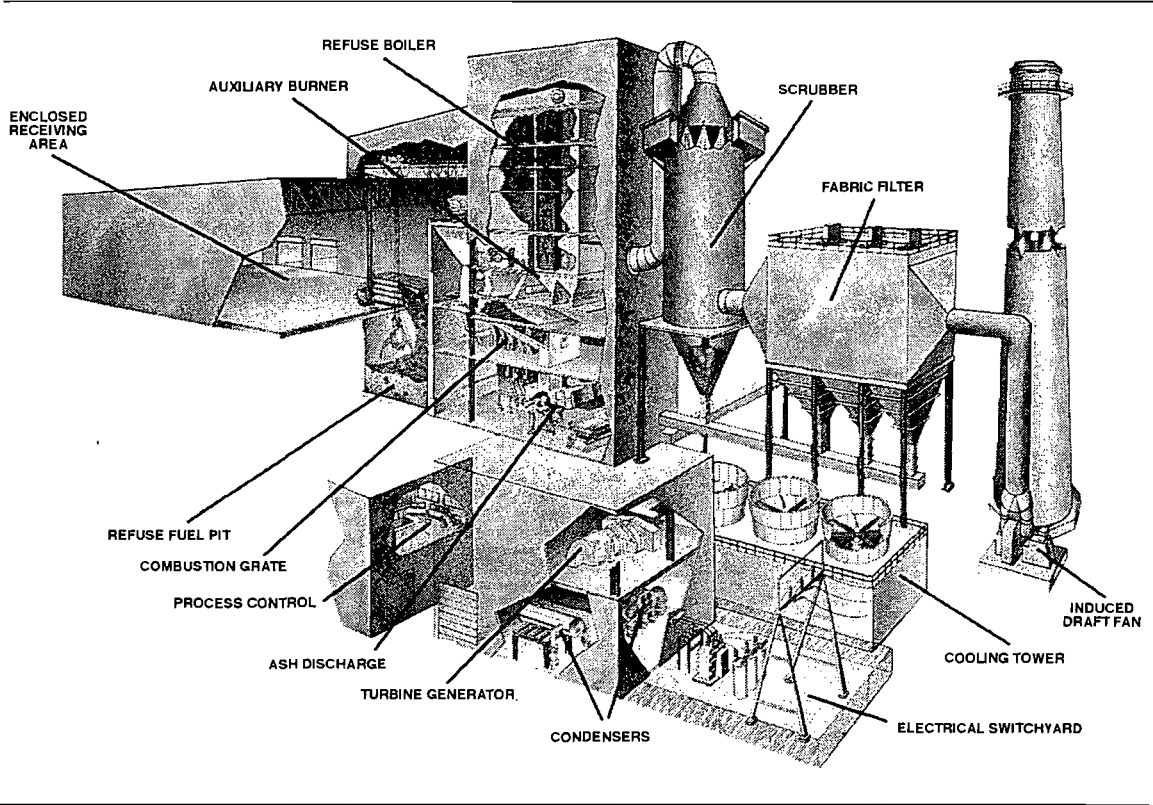


Figure 3-1: General Process Schematic

DESCRIPTION OF INSTALLATION

3-2

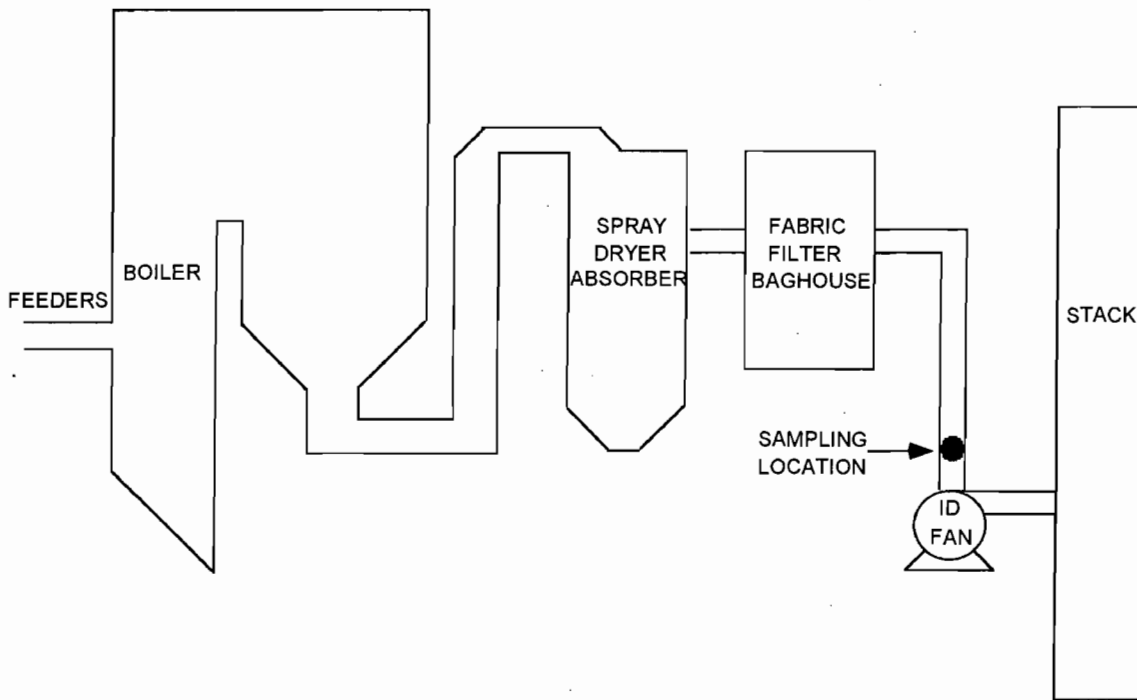


Figure 3-2: Process Schematic

DESCRIPTION OF INSTALLATION

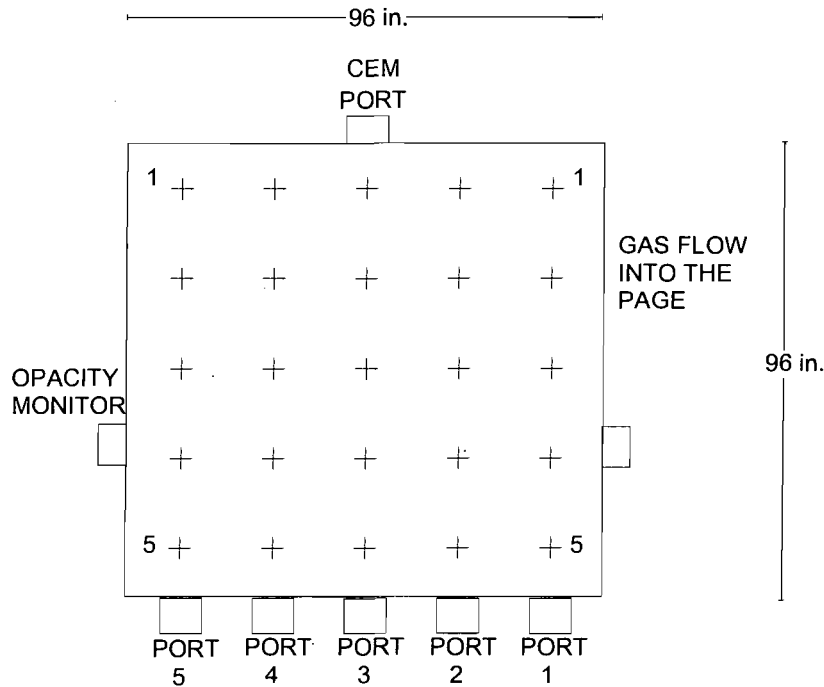
3-3

DESCRIPTION OF SAMPLING LOCATION(S)

Sampling point locations were determined according to EPA Method 1. Table 3-1 outlines the sampling point configurations. Figure 3-3 illustrates the sampling points and orientation of sampling ports for the source tested in the program.

**Table 3-1:
Sampling Points**

Location	Constituent	Method	Run No.	Ports	Points per Port	Minutes per Point	Total Minutes	Figure
Unit 2 FF Outlet	Mercury	29	1-3	5	5	5	125	3-3



Sampling Point	Port to Point Distance (in.)
1	86.4
2	67.2
3	48.0
4	28.8
5	9.6

Equivalent Duct diameters upstream from flow disturbance (A): 0.5 Limit: 0.5
 Equivalent Duct diameters downstream from flow disturbance (B): 2.0 Limit: 2.0

Figure 3-3: Unit 2 FF Outlet Sampling Point Determination (EPA Method 1)

METHODOLOGY

4-1

Clean Air Engineering followed procedures as detailed in U.S. Environmental Protection Agency (EPA) Methods 1, 2, 3, 3B, 4 and 29. The following table summarizes the methods and their respective sources.

**Table 4-1:
Summary of Sampling Procedures**

Title 40 CFR Part 60 Appendix A

Method 1	"Sample and Velocity Traverses for Stationary Sources"
Method 2	"Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)"
Method 3	"Gas Analysis for the Determination of Dry Molecular Weight"
Method 3B	"Gas Analysis for the Determination of Emission Rate Correction Factor or Excess Air"
Method 4	"Determination of Moisture Content in Stack Gases"
Method 29	"Determination of Metals Emissions from Stationary Sources"

These methods appear in detail in Title 40 of the Code of Federal Regulations (CFR) and on the World Wide Web at <http://www.cleanair.com>.

Diagrams of the sampling apparatus and major specifications of the sampling, recovery and analytical procedures are summarized for each method in Appendix A.

CleanAir followed specific quality assurance and quality control (QA/QC) procedures as outlined in the individual methods and in EPA "Quality Assurance Handbook for Air Pollution Measurement Systems: Volume III Stationary Source-Specific Methods", EPA/600/R-94/038C. Additional QA/QC methods, as prescribed in CleanAir's internal Quality Manual, were also followed. Results of all QA/QC activities performed by CleanAir are summarized in Appendix D.

End of Section 4 -Methodology

WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-5

APPENDIX

5-1

TEST METHOD SPECIFICATIONS.....	A
SAMPLE CALCULATIONS.....	B
PARAMETERS.....	C
QA/QC DATA.....	D
FIELD DATA.....	E
FIELD DATA PRINTOUTS.....	F
LABORATORY DATA.....	G
PLANT DATA.....	H

WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-5

TEST METHOD SPECIFICATIONS

A

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Specification Sheet for

EPA Method 29

Source Location Name(s) Unit 2 FF Outlet
 Pollutant(s) to be Determined Mercury
 Other Parameters to be Determined from Train Gas Density, Moisture, Flow Rate

	<u>Standard Method Specification</u>	<u>Actual Specification Used</u>
Pollutant Sampling Information		
Duration of Run	N/A	125 minutes
No. of Sample Traverse Points	N/A	25
Sample Time per Point	N/A	5 minutes
Sampling Rate	Isokinetic (90-110%)	Isokinetic (90-110%)
Sampling Probe		
Nozzle Material	Borosilicate or Quartz Glass	Borosilicate Glass
Nozzle Design	Button-Hook or Elbow	Button-Hook
Probe Liner Material	Borosilicate or Quartz Glass	Borosilicate Glass
Effective Probe Length	N/A	8 feet
Probe Temperature Set-Point	248°F±25°F	248°F±25°F
Velocity Measuring Equipment		
Pitot Tube Design	Type S	Type S
Pitot Tube Coefficient	N/A	0.82
Pitot Tube Calibration by	Geometric or Wind Tunnel	Wind-Tunnel
Pitot Tube Attachment	Attached to Probe	Attached to Probe
Metering System Console		
Meter Type	Dry Gas Meter	Dry Gas Meter
Meter Accuracy	±2%	±1%
Meter Resolution	N/A	0.01 cubic feet
Meter Size	N/A	0.1 dcf/revolution
Meter Calibrated Against	Wet Test Meter or Standard DGM	Wet Test Meter
Pump Type	N/A	Rotary Vane
Temperature Measurements	N/A	Type K Thermocouple/Pyrometer
Temperature Resolution	5.4°F	1.0°F
ΔP Differential Pressure Gauge	Inclined Manometer or Equivalent	Inclined Manometer
ΔH Differential Pressure Gauge	Inclined Manometer or Equivalent	Inclined Manometer
Barometer	Mercury or Aneroid	Digital Barometer calibrated w/Mercury Aneroid
Filter Description		
Filter Location	After Probe	Exit of Probe
Filter Holder Material	Borosilicate Glass	Borosilicate Glass
Filter Support Material	Teflon (or other non-metallic)	Teflon
Cyclone Material	N/A	None
Filter Heater Set-Point	248°F±25°F	248°F±25°F
Filter Material	Quartz or Glass Fiber	Quartz Fiber
Other Components		
Description	N/A	N/A
Location	N/A	N/A
Operating Temperature	N/A	N/A

Specification Sheet for

EPA Method 29

Impinger Train Description

Type of Glassware Connections
 Connection to Probe or Filter by
 Number of Impingers
 Impinger Stem Types

Impinger 1
 Impinger 2
 Impinger 3
 Impinger 4
 Impinger 5
 Impinger 6
 Impinger 7
 Impinger 8

Gas Density Determination

Sample Collection
 Sample Collection Medium
 Sample Analysis

Sample Recovery Information

Probe Brush Material
 Probe Rinse Reagent
 Probe Rinse Wash Bottle Material
 Probe Rinse Storage Container
 Filter Recovered?
 Filter Storage Container
 Impinger Contents Recovered?
 Impinger Rinse Reagent
 Impinger Wash Bottle
 Impinger Storage Container

Analytical Information

Method 4 H₂O Determination by
 Filter Preparation Conditions
 Front-Half Rinse Preparation
 Back-Half Analysis
 Additional Analysis

Standard Method Specification

Ground Glass or Equivalent
 Direct Glass Connection
 7

Modified Greenburg-Smith
 Modified Greenburg-Smith
 Greenburg-Smith
 Modified Greenburg-Smith
 Modified Greenburg-Smith
 Modified Greenburg-Smith
 Modified Greenburg-Smith

Multi-point integrated
 Flexible Gas Bag
 Orsat or Fyrite Analyzer

Non-metallic swab or bristle
 0.1N Nitric Acid
 Glass or Teflon
 Polyethylene or glass
 Yes
 Petri Dish - Glass or Polystyrene
 Yes
 See Method 29 Recovery Flow Chart
 Glass or Teflon
 See Recovery Flow Chart

Volumetric or Gravimetric
 See Method 29 Analytical Flow Chart
 See Method 29 Analytical Flow Chart
 See Method 29 Analytical Flow Chart
 None

Actual Specification Used

Screw Joint with Silicone Gasket
 Direct Glass Connection
 7

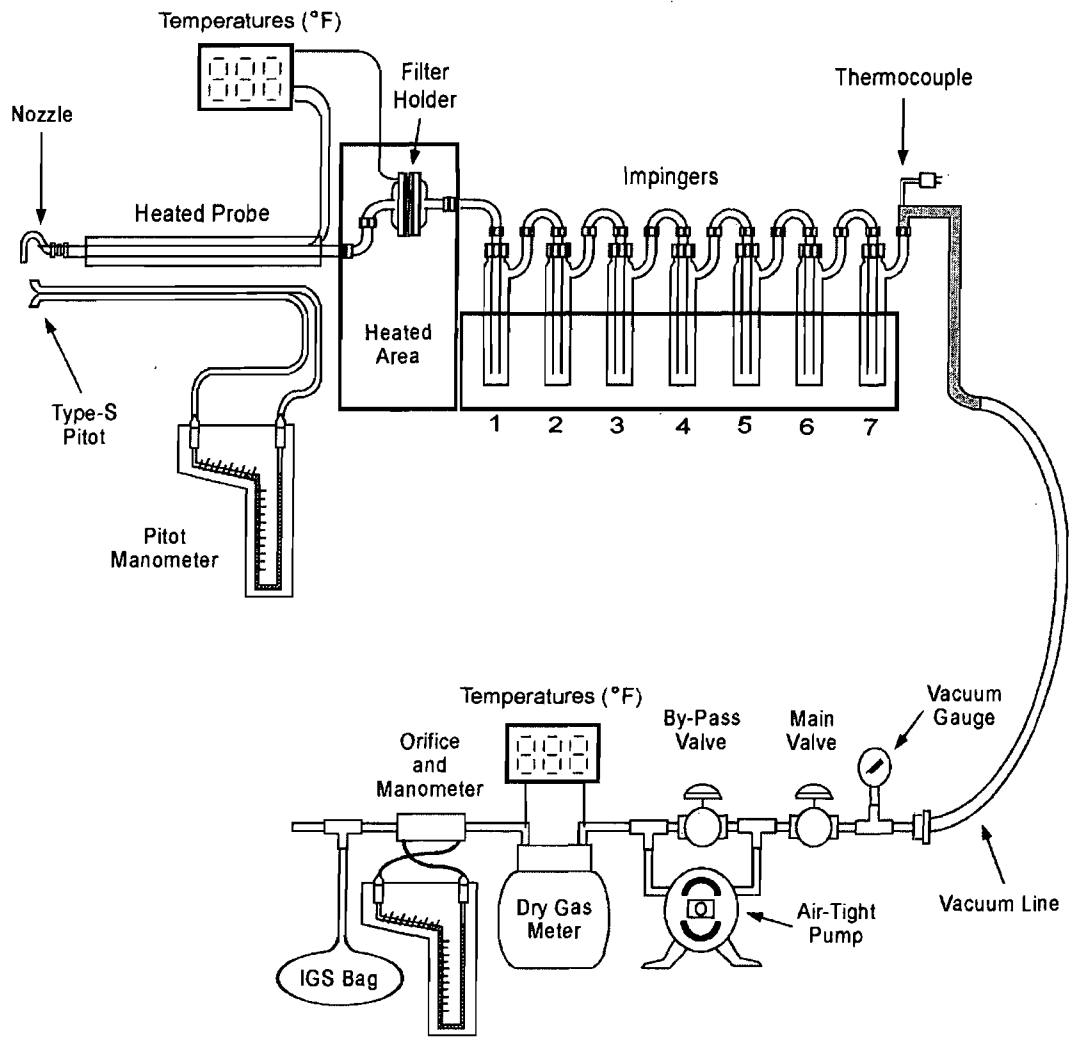
Modified Greenburg-Smith
 Modified Greenburg-Smith
 Greenburg-Smith
 Modified Greenburg-Smith
 Modified Greenburg-Smith
 Modified Greenburg-Smith
 Modified Greenburg-Smith

Multi-Point Integrated
 Vinyl Bag
 Orsat

Teflon Mat
 0.1 N Nitric Acid
 Teflon
 Polyethylene
 Yes
 Polyethylene
 Yes
 See Recovery Flow Chart
 Teflon
 See Recovery Flow Chart

Gravimetric and Volumetric
 For Metals Analysis
 See Analytical Flow Chart
 See Analytical Flow Chart
 None

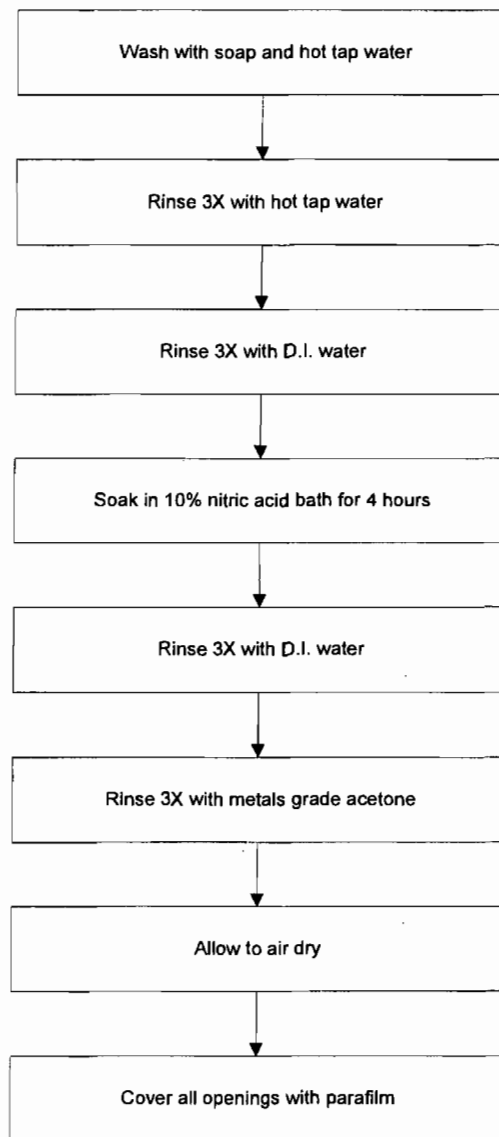
EPA Method 29 Sampling Train Configuration



Impinger Contents

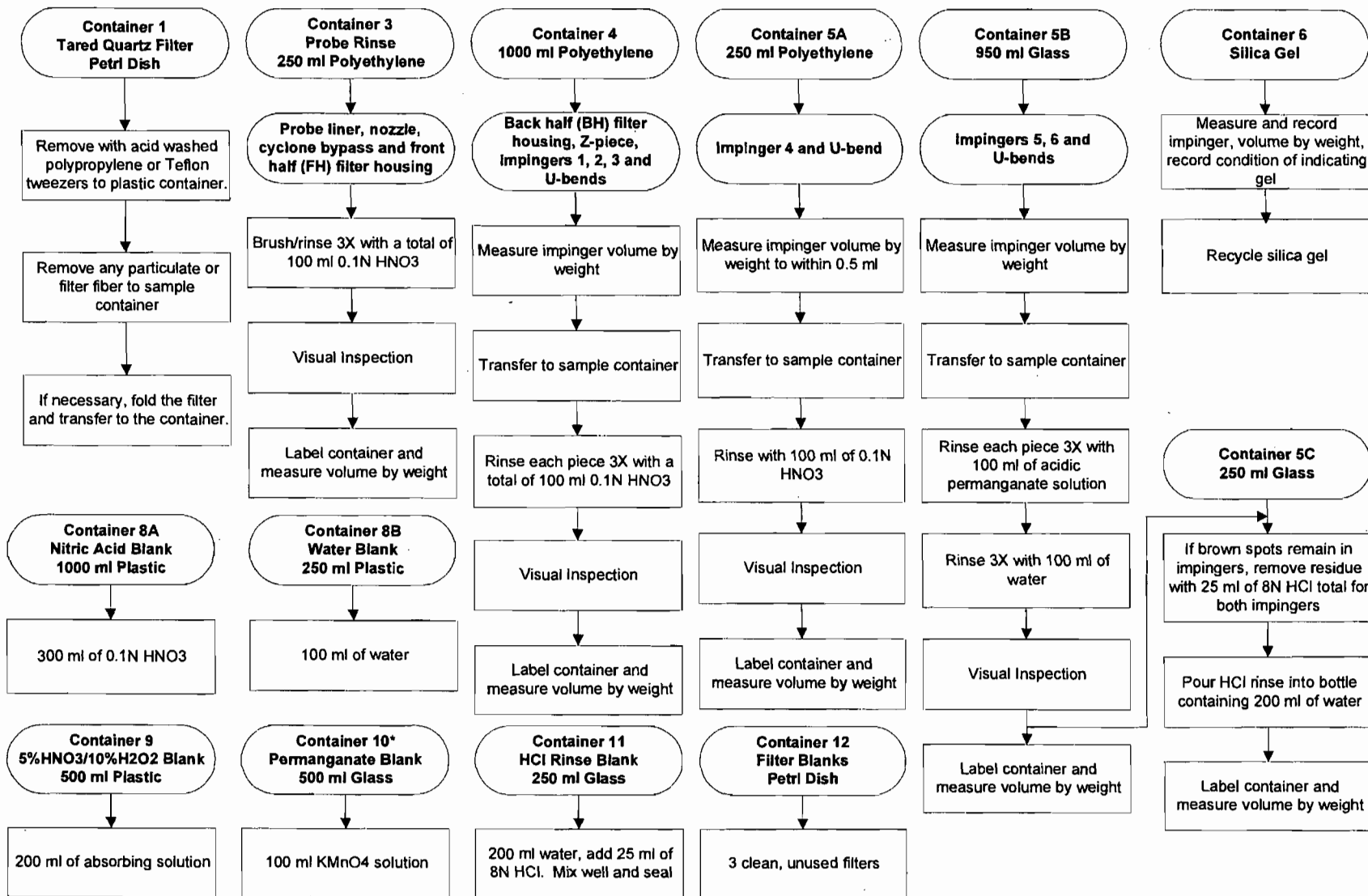
Impinger 1	Empty
Impinger 2	100 ml 5% HNO ₃ /10% H ₂ O ₂
Impinger 3	100 ml 5% HNO ₃ /10% H ₂ O ₂
Impinger 4	Empty
Impinger 5	100 ml 4% KMnO ₄ /10% H ₂ SO ₄
Impinger 6	100 ml 4% KMnO ₄ /10% H ₂ SO ₄
Impinger 7	Silica Gel

EPA Method 29 Glassware Preparation Procedures

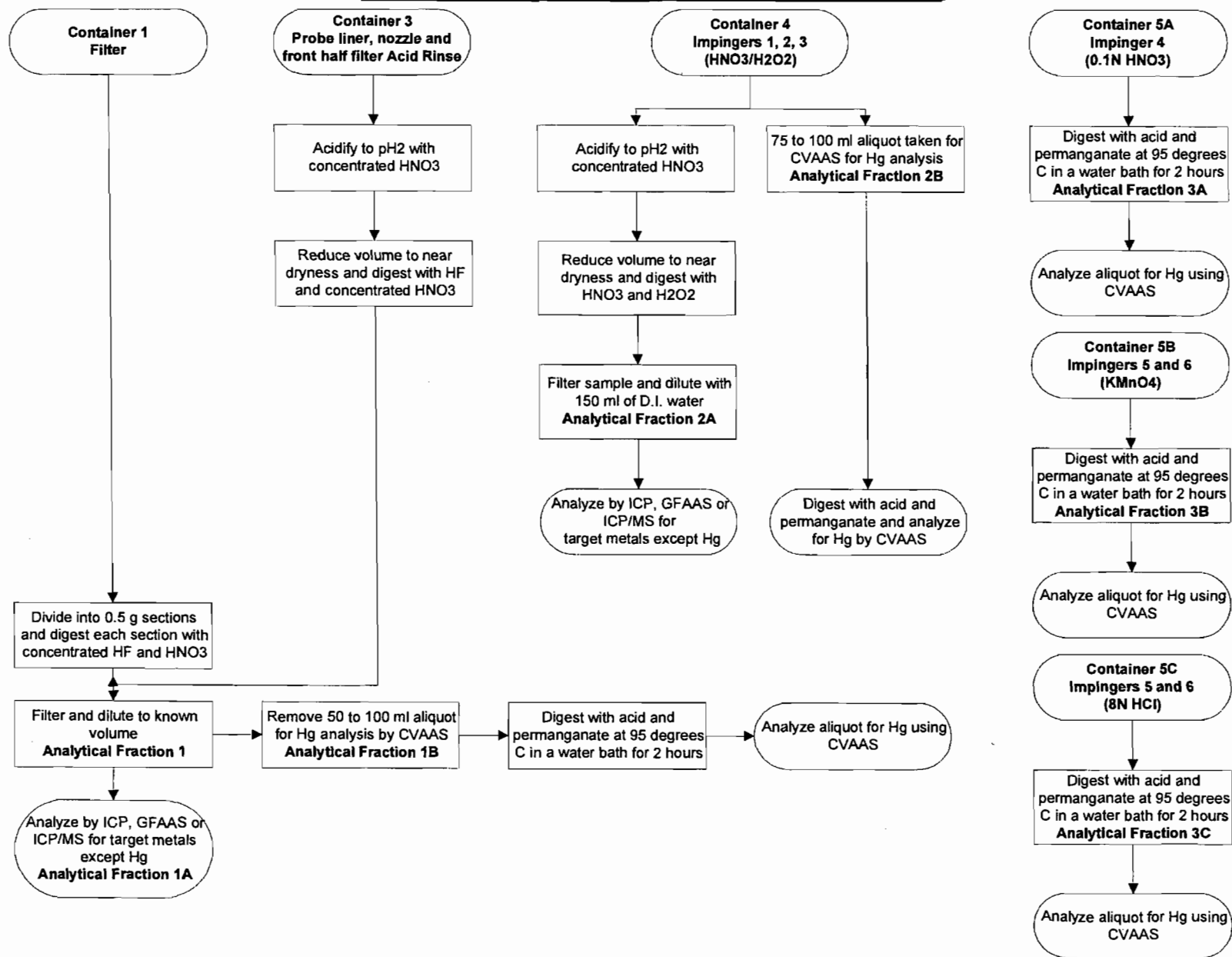


**EPA Method 29
Sample Recovery Flowchart
(Includes Mercury)**

- Tare all sample containers before sample collection
- Mark all liquid levels and final weights on the outside of each sample container
- Seal all sample containers with Teflon tape
- If recycling, bake silica gel for two hours at 350 degrees F (175 degrees C)
- Collect one complete blank set per field test



**EPA Method 29
Analytical Flowchart
(includes Mercury)**



WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-5

SAMPLE CALCULATIONS

B

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**USEPA Method 29 (Mercury)
 Sampling, Velocity and Moisture Sample Calculations**

Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

061410 111812
 P

1. Volume of water collected (wscf)

$$V_{wstd} = (0.04706)(V_{lc})$$

Where:

V_{lc}	= total volume of liquid collected in impingers and silica gel (ml)	=	518.3	ml
0.04706	= ideal gas conversion factor (ft ³ water vapor/ml or gm)	=	0.04706	ft ³ /ml
V_{wstd}	= volume of water vapor collected at standard conditions (ft ³)	=	24.39	ft ³

2. Volume of gas metered, standard conditions (dscf)

$$V_{mstd} = \frac{(17.64)(V_m) \left(P_{bar} + \frac{\Delta H}{13.6} \right) (Y_d)}{(460 + T_m)}$$

Where:

P_{bar}	= barometric pressure (in. Hg)	=	29.88	in. Hg
T_m	= average dry gas meter temperature (°F)	=	89.30	°F
V_m	= volume of gas sample through the dry gas meter at meter conditions (dcf)	=	81.36	dcf
Y_d	= gas meter correction factor (dimensionless)	=	0.9936	
ΔH	= average pressure drop across meter box orifice (in. H ₂ O)	=	1.28	in. H ₂ O
17.64	= standard temperature to pressure ratio (°R/in. Hg)	=	17.64	°R/in. Hg
13.6	= conversion factor (in. H ₂ O/in. Hg)	=	13.6	in.H ₂ O/in. Hg
460	= °F to °R conversion constant	=	460	
V_{mstd}	= volume of gas sampled through the dry gas meter at standard conditions (dscf)	=	77.819	dscf

3. Sample gas pressure (in. Hg)

$$P_s = P_{bar} + \left(\frac{P_g}{13.6} \right)$$

Where:

P_{bar}	= barometric pressure (in. Hg)	=	29.88	in. Hg
P_g	= sample gas static pressure (in. H ₂ O)	=	-9.10	in. H ₂ O
13.6	= conversion factor (in. H ₂ O/in. Hg)	=	13.6	in. H ₂ O/in. Hg
P_s	= absolute sample gas pressure (in. Hg)	=	29.21	in. Hg

4. Actual water vapor pressure at sample gas temperature less than 212°F (in. Hg)

$$P_v = \frac{e^{\left(\frac{18.3036 - \frac{3816.44}{\frac{5}{9}(T_s - 32) + 273.15 - 46.13}}{25.4} \right)}}{25.4}$$

Where:

T_s	= average sample gas temperature (°F)	=	309.24	°F
18.3036	= Antoine coefficient	=	18.3036	°K
3816.44	= Antoine coefficient	=	3816.44	°K
273.15	= temperature conversion factor	=	273.15	°K
46.13	= Antoine coefficient	=	46.13	°K
25.4	= conversion factor	=	25.4	mm Hg/in. Hg
5/9	= Fahrenheit to Celsius conversion factor	=	5/9	°C/°F
32	= temperature conversion (°F)	=	32	°F
P_v	= vapor pressure, actual (in. Hg)	=	29.21	in. Hg

5. Water vapor pressure at gas temperature greater than 212°F (in. Hg)

$$P_v = P_s$$

Where:

P_s	= absolute sample gas pressure (in. Hg)	=	29.21	in. Hg
P_v	= water vapor pressure, actual (in. Hg)	=	29.21	in. Hg

6. Moisture measured in sample (% by volume)

$$B_{wo} = \frac{V_{wstd}}{(V_{mstd} + V_{wstd})}$$

Where:

V_{mstd}	= volume of gas sampled through the dry gas meter at standard conditions (dscf)	=	77.819	dscf
V_{wstd}	= volume of water collected at standard conditions (scf)	=	24.39	scf
B_{wo}	= proportion of water measured in the gas stream by volume	=	0.2386	
		=	23.86	%

7. Saturated moisture content (% by volume)

$$B_{ws} = \frac{P_v}{P_s}$$

Where:

P_s	= absolute sample gas pressure (in. Hg)	=	29.21	in. Hg
P_v	= water vapor pressure, actual (in. Hg)	=	29.21	in. Hg
B_{ws}	= proportion of water vapor in the gas stream by volume at saturated conditions	=	1.0000	
		=	100.00	%

8. Actual water vapor in gas (% by volume)

$$B_w = \text{MINIMUM} [B_{wo}, B_{ws}]$$

Where:

B_{ws}	= proportion of water vapor in the gas stream by volume at saturated conditions	=	1.0000	
B_{wo}	= proportion of water measured in the gas stream by volume	=	0.2386	
B_w	= actual water vapor in gas	=	0.2386	%
		=	23.86	%

9. Nitrogen (plus carbon monoxide) in gas stream (% by volume, dry)

$$N_2 + CO = 100 - CO_2 - O_2$$

Where:

CO_2	= proportion of carbon dioxide in the gas stream by volume (%)	=	9.6	%
O_2	= proportion of oxygen in the gas stream by volume (%)	=	9.0	%
100	= conversion factor (%)	=	100	%
N_2+CO	= proportion of nitrogen and CO in the gas stream by volume (%)	=	81.40	%

10. Molecular weight of dry gas stream (lb/lb-mole)

$$M_d = (M_{CO_2}) \frac{(CO_2)}{(100)} + (M_{O_2}) \frac{(O_2)}{(100)} + (M_{N_2+CO}) \frac{(N_2 + CO)}{(100)}$$

Where:

M_{CO_2}	= molecular weight of carbon dioxide (lb/lb-mole)	=	44.00	lb/lb-mole
M_{O_2}	= molecular weight of oxygen (lb/lb-mole)	=	32.00	lb/lb-mole
M_{N_2+CO}	= molecular weight of nitrogen and carbon monoxide (lb/lb-mole)	=	28.00	lb/lb-mole
CO_2	= proportion of carbon dioxide in the gas stream by volume (%)	=	9.6	%
O_2	= proportion of oxygen in the gas stream by volume (%)	=	9.0	%
N_2+CO	= proportion of nitrogen and CO in the gas stream by volume (%)	=	81.4	%
100	= conversion factor (%)	=	100	%
M_d	= dry molecular weight of sample gas (lb/lb-mole)	=	29.89	lb/lb-mole

11. Molecular weight of sample gas (lb/lb-mole)

$$M_s = (M_d)(1 - B_w) + (M_{H_2O})(B_w)$$

Where:

B_w	= proportion of water vapor in the gas stream by volume	=	0.2386	
M_d	= dry molecular weight of sample gas (lb/lb-mole)	=	29.89	lb/lb-mole
M_{H_2O}	= molecular weight of water (lb/lb-mole)	=	18.00	lb/lb-mole
M_s	= molecular weight of sample gas, wet basis (lb/lb-mole)	=	27.05	lb/lb-mole

12. Velocity of sample gas (ft/sec)

$$V_s = (K_p)(C_p)(\sqrt{\Delta P}) \left(\sqrt{\frac{(T_s + 460)}{(M_s)(P_s)}} \right)$$

Where:

K_p	= velocity pressure constant	=	85.49	
C_p	= pitot tube coefficient	=	0.82	
M_s	= wet molecular weight of sample gas, wet basis (lb/lb-mole)	=	27.05	lb/lb-mole
P_s	= absolute sample gas pressure (in. Hg)	=	29.21	in. Hg
T_s	= average sample gas temperature (°F)	=	309.24	°F
$\sqrt{\Delta P}$	= average square roots of velocity heads of sample gas (in. H ₂ O)	=	0.691	$\sqrt{\text{in. H}_2\text{O}}$
460	= °F to °R conversion constant	=	460	
V_s	= sample gas velocity (ft/sec)	=	47.81	ft/sec

13. Volumetric flow rate of sample gas at actual gas conditions (acfm)

$$Q_a = (60)(A_s)(V_s)$$

Where:

A_s	= cross sectional area of sampling location (ft ²)	=	64.00	ft ²
V_s	= sample gas velocity (ft/sec)	=	47.81	ft/sec
60	conversion factor (sec/min)	=	60	sec/min
Q_a	= volumetric flow rate at actual conditions (acfm)	=	183,571	acfm

14. Total flow of sample gas (scfm)

$$Q_s = (Q_a) \left(\frac{P_s}{29.92} \right) \left(\frac{68 + 460}{T_s + 460} \right)$$

Where:

Q_a	= volumetric flow rate at actual conditions (acfm)	=	183,571	acfm
P_s	= absolute sample gas pressure (in. Hg)	=	29.21	in. Hg
29.92	= standard pressure (in. Hg)	=	29.92	in. Hg
T_s	= average sample gas temperature (°F)	=	309.2	°F
68	= standard temperature (°F)	=	68	°F
460	= °F to °R conversion constant	=	460	
Q_s	= volumetric flow rate at standard conditions, wet basis (scfm)	=	123,016	scfm

15. Dry flow of sample gas (dscfm)

$$Q_{std} = (Q_s)(1 - B_w)$$

Where:

B_w	= proportion of water vapor in the gas stream by volume	=	0.2386	
Q_s	= volumetric flow rate at standard conditions, wet basis (scfm)	=	123,016	scfm
Q_{std}	= volumetric flow rate at standard conditions, dry basis (dscfm)	=	93,659	dscfm

16. Dry flow of sample gas corrected to 7%O₂ (dscfm)

$$Q_{std7} = (Q_{std}) \left(\frac{20.9 - O_2}{20.9 - 7} \right)$$

Where:

Q _{std}	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 93,659	dscfm
O ₂	= proportion of oxygen in the gas stream by volume (%)	= 9.0	%
20.9	= oxygen content of ambient air (%)	= 20.9	%
7	= oxygen content of corrected gas (%)	= 7.0	%
Q _{std7}	= volumetric flow rate at STP and 7%O ₂ , dry basis (dscfm)	= 79,959	dscfm

17. Hourly time basis conversion of volumetric flow rate (Q_{std} example)

$$Q_{std-hr} = (Q_{std-min})(60)$$

Where

Q _{std-min}	= volumetric flow rate, english units (ft ³ /min)	= 93,659	dscfm
60	= conversion factor (min/hr)	= 60	min/hr
Q _{std-hr}	= volumetric flow rate, hourly basis (dscf/hr)	= 5,619,567	dscf/hr

18. Metric Conversion of Gas Volumes (Q_{std} example)

$$Q_{std-metric} = (Q_{std-english}) \left(\frac{60}{35.31} \right)$$

Where:

Q _{std-english}	= volumetric flow rate, english units (ft ³ /min)	= 93,659	dscfm
35.31	= conversion factor (ft ³ /m ³)	= 35.31	ft ³ /m ³
60	= conversion factor (min/hr)	= 60	min/hr
Q _{std-metric}	= volumetric flow rate, metric units (m ³ /hr)	= 159,149	dry std m ³ /hr

19. Standard to Normal Conversion of Gas Volumes (Q_{std} example)

$$Q_{Normal} = (Q_{std-metric}) \left(\frac{32 + 460}{68 + 460} \right)$$

Where:

Q _{std-metric}	= volumetric flow rate, metric units (dry std m ³ /hr)	= 159,149	dry std m ³ /hr
32	= normal temperature (°F)	= 32	°F
68	= standard temperature (°F)	= 68	°F
460	= standard temperature in Rankine (68°F)	= 460	
Q _{Normal}	= volumetric flow rate, metric units (dry Nm ³ /hr)	= 148,298	dry Nm ³ /hr

20. Percent isokinetic (%)

$$I = \frac{(0.09450)(\overline{T_s} + 460)(V_{mstd})}{(P_s)(V_s)\left(\frac{D_n^2(\pi)}{(144)(4)}\right)(\Theta)(1 - B_w)}$$

Where:

D_n	= diameter of nozzle (in)	=	0.273	in.
B_w	= proportion of water vapor in the gas stream by volume	=	0.2386	
P_s	= absolute sample gas pressure (in. Hg)	=	29.21	in. Hg
T_s	= average sample gas temperature (°F)	=	309.2	°F
V_{mstd}	= volume of gas sample through the dry gas meter at standard conditions (dscf)	=	77.819	dscf
V_s	= sample gas velocity (ft/sec)	=	47.81	ft/sec
θ	= total sampling time (min)	=	125	min
0.0945	= conversion constant	=	0.0945	
460	= °F to °R conversion constant	=	460	
I	= percent of isokinetic sampling (%)	=	104.71	%

21. Alternative Method 5 Post-Test Meter Calibration Factor

$$Y_{qa} = \frac{\Theta}{V_m} \sqrt{\frac{(0.0319)(T_m + 460)(28.96)}{(\Delta H_{\Theta})(P_{bar} + \frac{\Delta H}{13.6})(M_d)}} (\sqrt{\Delta H})_{avg}$$

Where:

θ	= total sampling time (min)	=	125	min
V_m	= volume of gas sample through the dry gas meter at meter conditions (dcf)	=	81.36	dcf
T_m	= average dry gas meter temperature (°F)	=	89.30	°F
ΔH_{Θ}	= dry gas meter orifice coefficient	=	1.7678	
P_{bar}	= barometric pressure (in. Hg)	=	29.88	in. Hg
ΔH	= average pressure drop across meter box orifice (in. H ₂ O)	=	1.280	in. H ₂ O
M_d	= dry molecular weight of sample gas (lb/lb-mole)	=	29.89	lb/lb-mole
$\sqrt{\Delta H}_{avg}$	= average of square root of pressure drop across meter orifice	=	1.128	$\sqrt{\text{in. H}_2\text{O}}$
0.0319	= conversion constant	=	0.0319	
28.96	= molecular weight of ambient air (lb/lb-mole)	=	28.96	lb/lb-mole
13.6	= conversion factor (in. H ₂ O/in. Hg)	=	13.6	in. H ₂ O/in. Hg
460	= °F to °R conversion constant	=	460	
Y_{qa}	= alternative Method 5 post-test meter calibration factor	=	0.9805	

LOGIC FOR TREATING DETECTION LIMITS

(mercury only)

1. Logic for Determining Total Blank ($m_{\text{Total-B}}$) from 5 Fractions

	CASE 1	CASE 2	CASE 3
	All 5 fractions are D.	1 to 4 fractions are ND	All 5 fractions are ND
Rule			
$ND = 0$	$m_{\text{Total-B}} = \text{Sum D, 1-5}$	$m_{\text{Total-B}} = \text{Sum D}$	$m_{\text{Total-B}} = < \text{Sum ND}$
$ND = 1x$	$m_{\text{Total-B}} = \text{Sum D, 1-5}$	$m_{\text{Total-B}} = \text{Sum D}$	$m_{\text{Total-B}} = < \text{Sum ND}$
$ND = 0.5x$	$m_{\text{Total-B}} = \text{Sum D, 1-5}$	$m_{\text{Total-B}} = \text{Sum D}$	$m_{\text{Total-B}} = < 0.5 \text{ Sum ND}$

2. Logic for Determining Total Sample ($m_{\text{Total-S}}$) from 5 Fractions

	CASE 1	CASE 2	CASE 3
	All 5 fractions are D.	1 to 4 fractions are ND	All 5 fractions are ND
Rule			
$ND = 0$	$m_{\text{Total-S}} = \text{Sum D, 1-5}$	$m_{\text{Total-S}} = \text{Sum D}$	$m_{\text{Total-S}} = < \text{Sum ND}$
$ND = 1x$	$m_{\text{Total-S}} = \text{Sum D, 1-5}$	$m_{\text{Total-S}} = < [\text{Sum D} + \text{Sum ND}]$	$m_{\text{Total-S}} = < \text{Sum ND}$
$ND = 0.5x$	$m_{\text{Total-S}} = \text{Sum D, 1-5}$	$m_{\text{Total-S}} = < [\text{Sum D} + 0.5 \text{ Sum ND}]$	$m_{\text{Total-S}} = < 0.5 \text{ Sum ND}$

3. Logic for Determining Maximum Allowable Blank Correction ($m_{\text{T-B-allow}}$)

	CASE 1	CASE 2	CASE 3	CASE 4
	All 5 fractions are D.	1 to 4 sample fractions are ND	All 5 fractions are ND	Any type of fractions
	$m_{\text{Total-B}} = D$	$m_{\text{Total-B}} = D$	$m_{\text{Total-B}} = D$	$m_{\text{Total-B}} = ND$
Rule				
$ND = 0$	$m_{\text{T-B-allow}} = \text{M29 Rule}$	$m_{\text{T-B-allow}} = \text{M29 Rule}^*$	$m_{\text{T-B-allow}} = 0$	$m_{\text{T-B-allow}} = 0$
$ND = 1x$	$m_{\text{T-B-allow}} = \text{M29 Rule}$	$m_{\text{T-B-allow}} = \text{M29 Rule}^*$	$m_{\text{T-B-allow}} = 0$	$m_{\text{T-B-allow}} = 0$
$ND = 0.5x$	$m_{\text{T-B-allow}} = \text{M29 Rule}$	$m_{\text{T-B-allow}} = \text{M29 Rule}^*$	$m_{\text{T-B-allow}} = 0$	$m_{\text{T-B-allow}} = 0$

* M29 rule using only detected sample quantities for logical comparisons.

4. Logic for Determining Blank-Corrected Sample Amount (m_n)

	CASE 1	CASE 2	CASE 3	CASE 4
	All 5 fractions are D.	1 to 4 sample fractions are ND	All 5 fractions are ND	Any type of fractions
	$m_{\text{Total-S}} - m_{\text{T-B-allow}} \geq \text{MIN}(\text{MDL})$	$m_{\text{Total-S}} - m_{\text{T-B-allow}} \geq \text{MIN}(\text{MDL})$	$m_{\text{Total-S}}$ and $m_{\text{T-B-allow}}$ anything	$m_{\text{Total-S}} - m_{\text{T-B-allow}} < \text{MIN}(\text{MDL})$
Rule				
$ND = 0$	$m_n = m_{\text{Total-S}} - m_{\text{T-B-allow}}$	$m_n = m_{\text{Total-S}} - m_{\text{T-B-allow}}$	$m_n = < m_{\text{Total-S}}$	$m_n = < \text{MIN}[\text{MDL}]$
$ND = 1x$	$m_n = m_{\text{Total-S}} - m_{\text{T-B-allow}}$	$m_n = < [m_{\text{Total-S}} - m_{\text{T-B-allow}}]$	$m_n = < m_{\text{Total-S}}$	$m_n = < \text{MIN}[\text{MDL}]$
$ND = 0.5x$	$m_n = m_{\text{Total-S}} - m_{\text{T-B-allow}}$	$m_n = < [m_{\text{Total-S}} - m_{\text{T-B-allow}}]$	$m_n = < m_{\text{Total-S}}$	$m_n = < \text{MIN}[\text{MDL}]$

Definitions and Notes

The term "Rule" refers to the rule being implemented for handling non-detectable quantities in summations.

MDL = minimum detection limit.

D = Detectable quantity reported as D.

ND = Non-Detectable quantity reported at a value of ND.

MIN[MDL] = lowest quantity of all detection limits for 5 fractions.

**USEPA Method 29
 Mercury Analyte Calculations**

Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

Note: Please see the preceding page concerning treatment of minimum detection limits and mathematical operations on values that are below minimum detection limits.

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 K

1. Total blank amount (µg)

$$m_{total-B} = \sum_{i=1}^n m_{i-B}$$

Where:

m_{1b-B}	= mercury amount in blank for Fraction 1b	=	<0.1000	µg
m_{2b-B}	= mercury amount in blank for Fraction 2b	=	<0.2000	µg
m_{3a-B}	= mercury amount in blank for Fraction 3a	=	<0.2000	µg
m_{3b-B}	= mercury amount in blank for Fraction 3b	=	<0.5000	µg
m_{3c-B}	= mercury amount in blank for Fraction 3c	=	<0.4000	µg
$m_{total-B}$	= total amount of mercury in blank	=	<1.4000	µg

2. Total sample amount (µg)

$$m_{total-S} = \sum_{i=1}^n m_{i-S}$$

Where:

m_{1b-S}	= mercury amount in sample for Fraction 1b	=	0.1204	µg
m_{2b-S}	= mercury amount in sample for Fraction 2b	=	42.0524	µg
m_{3a-S}	= mercury amount in sample for Fraction 3a	=	<0.2000	µg
m_{3b-S}	= mercury amount in sample for Fraction 3b	=	<0.5000	µg
m_{3c-S}	= mercury amount in sample for Fraction 3c	=	0.8843	µg
$m_{total-S}$	= total amount of mercury in sample	=	43.0571	µg

3. Allowable blank correction (µg)

$$m_{T-B-allow} = m_{total-B} \text{ if } m_{total-B} \leq 0.6$$

$$m_{T-B-allow} = \text{MAX} [0.6, \text{MIN} (m_{total-B}, 0.05 \times m_{total-S})] \text{ if } m_{total-B} > 0.6$$

Where:

$m_{total-B}$	= total amount of mercury in blank	=	<1.4000	µg
$m_{total-S}$	= total amount of mercury in sample	=	43.0571	µg
$0.05 \times m_{total-S}$	= 5% of $m_{total-S}$	=	2.1529	µg
MAX	= arithmetic operator that returns the maximum of two values			
MIN	= arithmetic operator that returns the minimum of two values			
$m_{T-B-allow}$	= total allowable blank correction	=	0.0000	µg

NOTE: In this case, the second criteria applies.

4. Sample corrected for allowable blank - Total (μg)

$$m_n = m_{\text{total-S}} - m_{\text{T-B-allow}}$$

Where:

$m_{\text{total-S}}$	= total amount of mercury in sample	=	43.0571	μg
$m_{\text{T-B-allow}}$	= total allowable blank correction	=	0.0000	μg
m_n	= total mercury in sample corrected for allowable blank	=	43.0571	μg

5. Sample corrected for allowable blank - Prorated for each fraction (μg)

$$m_{n-i} = \left(\frac{m_{i-S}}{m_{\text{total-S}}} \right) (m_n)$$

Where:

m_n	= total mercury in sample corrected for allowable blank	=	43.0571	μg
m_{1b-S}	= mercury amount in sample for Fraction 1b	=	0.1204	μg
m_{2b-S}	= mercury amount in sample for Fraction 2b	=	42.0524	μg
m_{3a-S}	= mercury amount in sample for Fraction 3a	=	<0.2000	μg
m_{3b-S}	= mercury amount in sample for Fraction 3b	=	<0.5000	μg
m_{3c-S}	= mercury amount in sample for Fraction 3c	=	0.8843	μg
$m_{\text{total-S}}$	= total amount of mercury in sample	=	43.0571	μg
m_{n-1b}	= mercury corrected for blank - prorated for Fraction 1b	=	0.1204	μg
m_{n-2b}	= mercury corrected for blank - prorated for Fraction 2b	=	42.0524	μg
m_{n-3a}	= mercury corrected for blank - prorated for Fraction 3a	=	<0.2000	μg
m_{n-3b}	= mercury corrected for blank - prorated for Fraction 3b	=	<0.5000	μg
m_{n-3c}	= mercury corrected for blank - prorated for Fraction 3c	=	0.8843	μg

**USEPA Method 29
 Mercury Sample Calculations**

Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

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 P_K

1. Mercury concentration (lb/dscf)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{2.205 \times 10^{-3}}{10^6} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 43.0571	μg
V_{mstd}	= volume metered, standard (dscf)	= 77.8189	dscf
2.205×10^{-3}	= conversion factor (lb/g)	= 2.205E-03	lb/g
10^6	= conversion factor ($\mu\text{g/g}$)	= 1.0E+06	$\mu\text{g/g}$
C_{sd}	= mercury concentration (lb/dscf)	= 1.2200E-09	lb/dscf

2. Mercury concentration ($\mu\text{g/dscm}$)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}} \right) (35.31)$$

Where:

m_n	= mercury collected in sample (total μg)	= 43.0571	μg
V_{mstd}	= volume metered, standard (dscf)	= 77.8189	dscf
35.31	= conversion factor (dscf/dscm)	= 35.31	dscf/dscm
C_{sd}	= mercury concentration ($\mu\text{g/dscm}$)	= 1.9537E+01	$\mu\text{g/dscm}$

3. Mercury concentration (mg/dscm)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{35.31}{1000} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 43.0571	μg
V_{mstd}	= volume metered, standard (dscf)	= 77.8189	dscf
35.31	= conversion factor (dscf/dscm)	= 35.31	dscf/dscm
1000	= conversion factor ($\mu\text{g/mg}$)	= 1000	$\mu\text{g/mg}$
C_{sd}	= mercury concentration (mg/dscm)	= 1.9537E-02	mg/dscm

4. Mercury concentration ($\mu\text{g}/\text{Nm}^3$ dry)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}} \right) (35.31) \left(\frac{68 + 460}{32 + 460} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 43.0571	μg
V_{mstd}	= volume metered, standard (dscf)	= 77.8189	dscf
35.31	= conversion factor (dscf/dscm)	= 35.31	dscf/dscm
68	= standard temperature ($^{\circ}\text{F}$)	= 68	$^{\circ}\text{F}$
32	= normal temperature ($^{\circ}\text{F}$)	= 32	$^{\circ}\text{F}$
460	= $^{\circ}\text{F}$ to $^{\circ}\text{R}$ conversion constant	= 460	

C_{sd}	= mercury concentration ($\mu\text{g}/\text{Nm}^3$ dry)	= 2.0967E+01	$\mu\text{g}/\text{Nm}^3$ dry
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5. Mercury concentration corrected to x% oxygen (lb/dscf example)

$$C_{sdx} = C_{sd} \left(\frac{20.9 - x}{20.9 - O_2} \right)$$

Where:

C_{sd}	= mercury concentration (lb/dscf)	= 1.2200E-09	lb/dscf
x	= oxygen content of corrected gas (%)	= 7.0	%
O_2	= proportion of oxygen in the gas stream by volume (%)	= 9.0	%
20.9	= oxygen content of ambient air (%)	= 20.9	%

C_{sdx}	= mercury concentration corrected to x% oxygen (lb/dscf)	= 1.4291E-09	lb/dscf @ x% O_2
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6. Mercury concentration corrected to y% carbon dioxide (lb/dscf example)

$$C_{sdy} = C_{sd} \left(\frac{y}{CO_2} \right)$$

Where:

C_{sd}	= mercury concentration (lb/dscf)	= 1.2200E-09	lb/dscf
y	= carbon dioxide content of corrected gas (%)	= 12.0	%
CO_2	= proportion of carbon dioxide in the gas stream by volume (%)	= 9.6	%

C_{sdy}	= mercury conc. corrected to y% carbon dioxide (lb/dscf)	= 1.5303E-09	lb/dscf @ y% CO_2
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7. Mercury concentration at actual gas conditions (lb/acf example)

$$C_a = C_{sd} \left(\frac{Q_{std}}{Q_a} \right)$$

Where:

C_{sd}	= mercury concentration (lb/dscf)	= 1.2200E-09	lb/dscf
Q_{std}	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 93,659	dscfm
Q_a	= volumetric flow rate at actual conditions (acfm)	= 183,571	acfm

C_a	= mercury concentration at actual gas conditions (lb/acf)	= 6.2246E-10	lb/acf
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8. Mercury emission rate (lb/hr)

$$E_{lb/hr} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{2.205 \times 10^{-3}}{10^6} \right) (Q_{std})(60)$$

Where:

m_n	= mercury collected in sample (total μg)	= 43.0571	μg
V_{mstd}	= volume metered, standard (dscf)	= 77.8189	dscf
2.205×10^{-3}	= conversion factor (lb/g)	= 2.205E-03	lb/g
10^6	= conversion factor ($\mu\text{g/g}$)	= 1.0E+06	$\mu\text{g/g}$
Q_{std}	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 93,659	dscfm
60	= conversion factor (min/hr)	= 60	min/hr
$E_{lb/hr}$	= mercury emission rate (lb/hr)	= 6.8560E-03	lb/hr

9. Mercury emission rate (g/s)

$$E_{g/s} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{Q_{std}}{(10^6)(60)} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 43.0571	μg
V_{mstd}	= volume metered, standard (dscf)	= 77.8189	dscf
Q_{std}	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 93,659	dscfm
10^6	= conversion factor ($\mu\text{g/g}$)	= 1.0E+06	$\mu\text{g/g}$
60	= conversion factor (sec/min)	= 60	sec/min
$E_{g/s}$	= mercury emission rate (g/s)	= 8.6369E-04	g/s

10. Mercury emission rate (Ton/yr)

$$E_{T/yr} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{2.205 \times 10^{-3}}{10^6} \right) (Q_{std})(60) \left(\frac{Cap}{2000} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 43.0571	μg
V_{mstd}	= volume metered, standard (dscf)	= 77.8189	dscf
2.205×10^{-3}	= conversion factor (lb/g)	= 2.205E-03	lb/g
10^6	= conversion factor ($\mu\text{g/g}$)	= 1.0E+06	$\mu\text{g/g}$
Q_{std}	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 93,659	dscfm
60	= conversion factor (min/hr)	= 60	min/hr
Cap	= capacity factor for process (hours operated/year)	= 8,760	hours/yr
2000	= conversion factor (lb/Ton)	= 2000	lb/Ton
$E_{T/yr}$	= mercury emission rate (Ton/yr)	= 3.0029E-02	Ton/yr

11. Mercury emission rate - Fd-based (lb/MMBtu)

$$E_{Fd} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{2.205 \times 10^{-3}}{10^6} \right) (F_d) \left(\frac{20.9}{20.9 - O_2} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 43.0571	μg
V_{mstd}	= volume metered, standard (dscf)	= 77.8189	dscf
2.205×10^{-3}	= conversion factor (lb/g)	= 2.205E-03	lb/g
10^6	= conversion factor ($\mu\text{g/g}$)	= 1.0E+06	$\mu\text{g/g}$
F_d	= ratio of gas volume to heat content of fuel (dscf/MMBtu)	= 9,570	dscf/MMBtu
O_2	= proportion of oxygen in the gas stream by volume (%)	= 9.0	%
20.9	= oxygen content of ambient air (%)	= 20.9	%
E_{Fd}	= mercury emission rate - Fd-based (lb/MMBtu)	= 2.0564E-05	lb/MMBtu

12. Mercury emission rate - Fc-based (lb/MMBtu)

$$E_{Fc} = \left(\frac{m_n}{V_{mstd}} \right) \left(\frac{2.205 \times 10^{-3}}{10^6} \right) (F_c) \left(\frac{100}{CO_2} \right)$$

Where:

m_n	= mercury collected in sample (total μg)	= 43.0571	μg
V_{mstd}	= volume metered, standard (dscf)	= 77.8189	dscf
2.205×10^{-3}	= conversion factor (lb/g)	= 2.205E-03	lb/g
10^6	= conversion factor ($\mu\text{g/g}$)	= 1.0E+06	$\mu\text{g/g}$
F_c	= ratio of gas volume to heat content of fuel (dscf/MMBtu)	= 1,820	dscf/MMBtu
CO_2	= proportion of oxygen in the gas stream by volume (%)	= 9.6	%
100	= conversion factor	= 100	
E_{Fc}	= mercury emission rate - Fc-based (lb/MMBtu)	= 2.3210E-05	lb/MMBtu

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WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-5

PARAMETERS

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Wheelabrator North Broward, Inc.
 Clean Air Project No: 10955
 Unit 2 FF Outlet

**USEPA Method 29 (Mercury)
 Sampling, Velocity and Moisture Parameters**

Run No.		1	2	3	Average
Date (2010)		May 25	May 25	May 25	
Start Time (approx.)		07:39	10:18	12:50	
Stop Time (approx.)		09:50	12:29	15:00	
Sampling Conditions					
Y _d	Dry gas meter correction factor	0.9936	0.9936	0.9936	
C _p	Pitot tube coefficient	0.8200	0.8200	0.8200	
P _g	Static pressure (in. H ₂ O)	-9.1000	-10.2000	-10.1000	
A _s	Sample location area (ft ²)	64.0000	64.0000	64.0000	
P _{bar}	Barometric pressure (in. Hg)	29.88	29.88	29.88	29.8800
D _n	Nozzle diameter (in.)	0.2730	0.2730	0.2730	
O ₂	Oxygen (dry volume %)	9.0333	9.0000	9.0000	9.0111
CO ₂	Carbon dioxide (dry volume %)	9.5667	9.8000	9.7667	9.7111
N ₂ +CO	Nitrogen plus carbon monoxide (dry volume %)	81.4000	81.2000	81.2333	81.2778
V _{lc}	Total Liquid collected (ml)	518.30	473.70	494.60	
V _m	Volume metered, meter conditions (ft ³)	81.3650	76.9400	78.9750	
T _m	Dry gas meter temperature (°F)	89.3000	95.7000	100.1800	
T _s	Sample temperature (°F)	309.2400	308.8000	308.7600	308.9333
ΔH	Meter box orifice pressure drop (in. H ₂ O)	1.2804	1.1340	1.1792	
θ	Total sampling time (min)	125.0	125.0	125.0	
Flow Results					
V _{wetd}	Volume of water collected (ft ³)	24.3912	22.2923	23.2759	23.3198
V _{metd}	Volume metered, standard (dscf)	77.8189	72.7131	74.0476	74.8599
P _a	Sample gas pressure, absolute (in. Hg)	29.2109	29.1300	29.1374	29.1594
P _v	Vapor pressure, actual (in. Hg)	29.2109	29.1300	29.1374	29.1594
B _{wo}	Moisture measured in sample (% by volume)	23.8638	23.4643	23.9160	23.7480
B _{ws}	Saturated moisture content (% by volume)	100.0000	100.0000	100.0000	100.0000
B _w	Actual water vapor in gas (% by volume)	23.8638	23.4643	23.9160	23.7480
√ΔP	Velocity head (√in. H ₂ O)	0.6912	0.6585	0.6766	0.6754
M _d	MW of sample gas, dry (lb/lb-mole)	29.8920	29.9280	29.9227	29.9142
M _w	MW of sample gas, wet (lb/lb-mole)	27.0541	27.1292	27.0712	27.0848
V _s	Velocity of sample (ft/sec)	47.8051	45.5279	46.8218	46.7183
%I	Isokinetic sampling (%)	104.7143	102.4266	101.9952	103.0453
Q _a	Volumetric flow rate, actual (acfm)	183,571	174,827	179,796	179,398
Q _s	Volumetric flow rate, standard (scfm)	123,016	116,898	120,257	120,057
Q _{std}	Volumetric flow rate, dry standard (dscfm)	93,659	89,469	91,496	91,542
Q _{std7}	Volumetric flow rate, dry std@7%O ₂ (dscfm)	79,959	76,596	78,332	78,295
Q _a	Volumetric flow rate, actual (acf/hr)	11,014,288	10,489,634	10,787,741	10,763,888
Q _s	Volumetric flow rate, standard (scf/hr)	7,380,938	7,013,904	7,215,429	7,203,424
Q _{std}	Volumetric flow rate, dry standard (dscf/hr)	5,619,567	5,368,143	5,489,788	5,492,500
Q _a	Volumetric flow rate, actual (m ³ /hr)	311,931	297,073	305,515	304,840
Q _s	Volumetric flow rate, standard (m ³ /hr)	209,033	198,638	204,345	204,005
Q _{std}	Volumetric flow rate, dry standard (dry m ³ /hr)	159,149	152,029	155,474	155,551
Q _{std7}	Volumetric flow rate, dry std@7%O ₂ (dry m ³ /hr)	135,869	130,154	133,104	133,042
Q _s	Volumetric flow rate, normal (Nm ³ /hr)	194,780	185,094	190,413	190,096
Q _{std}	Volumetric flow rate, dry normal (Nm ³ /hr)	148,298	141,663	144,874	144,945
Q _{std7}	Volumetric flow rate, dry normal @7%O ₂ (Nm ³ /hr)	126,605	121,280	124,028	123,971

Comments:

Average includes 3 runs.

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Wheelabrator North Broward, Inc.
 Clean Air Project No: 10955
 Unit 2 FF Outlet

**USEPA Method 29
 Mercury (Hg) Emission Parameters**

Run No.	1	2	3	Average	
Date (2010)	May 25	May 25	May 25		
Start Time (approx.)	07:39	10:18	12:50		
Stop Time (approx.)	09:50	12:29	15:00		
Process Conditions					
R _p	Steam Production Rate - (Klbs/hour)	185	184	184	184
P ₁	SDA Outlet Temperature - (°F)	319	320	320	320
F _d	Oxygen-based F-factor (dscf/MMBtu)	9,570	9,570	9,570	9,570
F _c	Carbon dioxide-based F-factor (dscf/MMBtu)	1,820	1,820	1,820	1,820
Cap	Capacity factor (hours/year)	8,760	8,760	8,760	8,760
Gas Conditions					
O ₂	Oxygen (dry volume %)	9.0333	9.0000	9.0000	9.0111
CO ₂	Carbon dioxide (dry volume %)	9.5667	9.8000	9.7667	9.7111
T _s	Sample temperature (°F)	309.2400	308.8000	308.7600	308.9333
B _w	Actual water vapor in gas (% by volume)	23.8638	23.4643	23.9160	23.7480
Gas Flow Rate					
Q _a	Volumetric flow rate, actual (acfm)	183,571	174,827	179,796	179,398
Q _s	Volumetric flow rate, standard (scfm)	123,016	116,898	120,257	120,057
Q _{std}	Volumetric flow rate, dry standard (dscfm)	93,659	89,469	91,496	91,542
Q _{std7}	Volumetric flow rate, dry std@7%O ₂ (dscfm)	79,959	76,596	78,332	78,295
Q _a	Volumetric flow rate, actual (acf/hr)	11,014,288	10,489,634	10,787,741	10,763,888
Q _s	Volumetric flow rate, standard (scf/hr)	7,380,938	7,013,904	7,215,429	7,203,424
Q _{std}	Volumetric flow rate, dry standard (dscf/hr)	5,619,567	5,368,143	5,489,788	5,492,500
Q _a	Volumetric flow rate, actual (m ³ /hr)	311,931	297,073	305,515	304,840
Q _s	Volumetric flow rate, standard (m ³ /hr)	209,033	198,638	204,345	204,005
Q _{std}	Volumetric flow rate, dry standard (dry m ³ /hr)	159,149	152,029	155,474	155,551
Q _{std7}	Volumetric flow rate, dry std@7%O ₂ (dry m ³ /hr)	135,869	130,154	133,104	133,042
Q _s	Volumetric flow rate, normal (Nm ³ /hr)	194,780	185,094	190,413	190,096
Q _{std}	Volumetric flow rate, dry normal (Nm ³ /hr)	148,298	141,663	144,874	144,945
Q _{std7}	Volumetric flow rate, dry normal @7%O ₂ (Nm ³ /hr)	126,605	121,280	124,028	123,971
Sampling Data					
V _{std}	Volume metered, standard (dscf)	77.8189	72.7131	74.0476	74.8599
%I	Isokinetic sampling (%)	104.7143	102.4266	101.9952	103.0453
Laboratory Data					
m _{n-1b}	Fraction 1B (µg)	0.1204	<0.1000	<0.1000	
m _{n-2b}	Fraction 2B (µg)	42.0524	20.5021	19.5846	
m _{n-3a}	Fraction 3A (µg)	<0.2000	<0.2000	<0.2000	
m _{n-3b}	Fraction 3B (µg)	<0.5000	<0.5000	<0.5000	
m _{n-3c}	Fraction 3C (µg)	0.8843	<0.4000	<0.4000	
m _n	Total matter corrected for allowable blanks (µg)	43.0571	20.5021	19.5846	
Mercury Results - Total					
C _{sd}	Concentration (lb/dscf)	1.2200E-09	6.2172E-10	5.8319E-10	8.0831E-10
C _{sd7}	Concentration @7% O ₂ (lb/dscf)	1.4291E-09	7.2621E-10	6.8121E-10	9.4550E-10
C _{sd12}	Concentration @12% CO ₂ (lb/dscf)	1.5303E-09	7.6129E-10	7.1655E-10	1.0027E-09
C _a	Concentration (lb/acf)	6.2246E-10	3.1817E-10	2.9678E-10	4.1247E-10
C _{sd}	Concentration (µg/dscm)	1.9537E+01	9.9559E+00	9.3390E+00	1.2944E+01
C _{sd7}	Concentration @7% O ₂ (µg/dscm)	2.2885E+01	1.1629E+01	1.0909E+01	1.5141E+01
C _{sd12}	Concentration @12% CO ₂ (µg/dscm)	2.4506E+01	1.2191E+01	1.1475E+01	1.6057E+01
C _{sd}	Concentration (mg/dscm)	1.9537E-02	9.9559E-03	9.3390E-03	1.2944E-02
C _{sd7}	Concentration @7% O ₂ (mg/dscm)	2.2885E-02	1.1629E-02	1.0909E-02	1.5141E-02
C _{sd12}	Concentration @12% CO ₂ (mg/dscm)	2.4506E-02	1.2191E-02	1.1475E-02	1.6057E-02
C _a	Concentration (µg/m ³ (actual,wet))	9.9679E+00	5.0950E+00	4.7526E+00	6.6052E+00
C _{sd}	Concentration (µg/Nm ³ dry)	2.0967E+01	1.0684E+01	1.0022E+01	1.3891E+01
C _{sd7}	Concentration @7% O ₂ (µg/Nm ³ dry)	2.4559E+01	1.2480E+01	1.1707E+01	1.6249E+01
C _{sd12}	Concentration @12% CO ₂ (µg/Nm ³ dry)	2.6299E+01	1.3083E+01	1.2314E+01	1.7232E+01
E _{lb/hr}	Rate (lb/hr)	6.8560E-03	3.3375E-03	3.2016E-03	4.4650E-03
E _{g/s}	Rate (g/s)	8.6369E-04	4.2044E-04	4.0333E-04	5.6249E-04
E _{T/yr}	Rate (Ton/yr)	3.0029E-02	1.4618E-02	1.4023E-02	1.9557E-02
E _{Fd}	Rate - Fd-based (lb/MMBtu)	2.0564E-05	1.0450E-05	9.8022E-06	1.3605E-05
E _{Fc}	Rate - Fc-based (lb/MMBtu)	2.3210E-05	1.1546E-05	1.0868E-05	1.5208E-05

Prepared by Clean Air Engineering Proprietary Software
 SS Metals-1 Version 2006-12a

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QA/QC _____
 Date _____

WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-5

QA/QC DATA

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Wheelabrator North Broward, Inc.
 Clean Air Project No: 10955
 Unit 2 FF Outlet

**USEPA Method 29 (Mercury)
 QA/QC Results**

Run No.	1	2	3
Date (2010)	May 25	May 25	May 25
Start Time (approx.)	07:39	10:18	12:50
Stop Time (approx.)	09:50	12:29	15:00
Total Duration of Test Run (min.)	131	131	130
Net Sampling Time (min.)	125	125	125

Sampling System Calibration Summary

D_n	Nozzle ID No:	273-1	273-1	273-1
	Nozzle Diameter (in):	0.273	0.273	0.273
C_p	Probe ID No:	67-8-18	67-8-18	67-8-18
	Pitot Coefficient:	0.8200	0.8200	0.8200
Y_d	Meter Box ID. No:	61-5	61-5	61-5
	Meter Box Y_d - Field Sheet	0.9936	0.9936	0.9936
	Meter Box Y_d - Database	0.9936	0.9936	0.9936
	Meter Box $\Delta H@$ - Field Sheet	1.7678	1.7678	1.7678
	Meter Box $\Delta H@$ - Database	1.7678	1.7678	1.7678

QA/QC

Final Leak Check

(a) 4% of Sampling Rate (cfm)	0.0260	0.0246	0.0253
(b) Allowable Rate from Method (cfm)	0.0200	0.0200	0.0200
Allowable Limit - minimum of a and b (cfm)	0.0200	0.0200	0.0200
Actual Final Leak Rate (cfm)	0.0150	0.0030	0.0020

Sample Volume

V_{mstd}	Minimum Volume Required (dscf)	30.00	30.00	30.00
	Actual Sample Volume (dscf)	77.819	72.713	74.048

Alternative Method 5 Post-Test Calibration (EPA ALT-009)

$\sqrt{\Delta H_{avg}}$	Average of Square Root of ΔH (in. W.C.)	1.1275	1.0618	1.0836
Y_{qa}	Alternative Meter Calibration Factor	0.9805	0.9817	0.9799
	Variation from full-test Y_d (average $\leq \pm 5\%$)	-1.3%	-1.2%	-1.4%

**Average
-1.3%**

Mean Isokinetic Sampling Rate Variation

%I	Minimum Allowable (%)	90	90	90
	Maximum Allowable (%)	110	110	110
	Actual Variation (%)	104.71	102.43	102.00

Point-by-Point Isokinetic Variation

	Number of points <90%	0	0	0
	Number of points >110%	0	0	0
	Number of points <80%	0	0	0
	Number of points >120%	0	0	0

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Nozzle Calibration Sheet

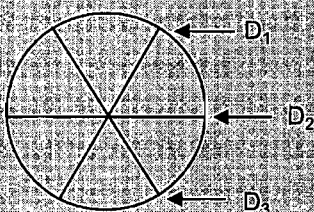
Client: <i>Wheelabrator</i>	Project Number: <i>10999</i>
Calibrated by: <i>C. Slimg</i>	Unit: <i>2</i>
Date: <i>5-24-10</i>	Runs: <i>1-3</i>

Nozzle Identification	D ₁ (inches)	D ₂ (inches)	D ₃ (inches)	ΔD (inches)	D _{ave} (inches)
<i>273-1</i>	<i>0.273</i>	<i>0.273</i>	<i>0.27 4</i>	<i>0.001</i>	<i>0.273</i>

D₁, D₂, D₃ = three nozzle diameter measurements

ΔD = maximum difference between any two diameters
ΔD = 0.004 inches*

D_{ave} = average of D₁, D₂, D₃



* (40 CFR 60, Appendix A, Method 5, Section 5.1)

QA/QC *CS*
Date *5/24/10*



Meter Box Full Test Calibration

Meter Box No: 61-5

Date of Calibration: 5/3/2010

Meter Box Y_d : 0.9936

Calibration Conducted by: OLEG LAVROV

Meter Box $\Delta H@$: 1.7676

Barometric Pressure: 29.00

				Standard Meter Gas Volume (ft ³)			Meter Box Gas Volume (ft ³)			Std. Meter Temperature (°F)			Meter Box Temperature (°F)			Time (min.)	Calibration Results	
Q	ΔH	ΔP	Y_{ds}	Initial	Final	V_{ds} Net	Initial	Final	V_d Net	T_{is} In	T_{os} Out	T_{ds} Avg.	T_i In	T_o Out	T_d Avg.	Θ	Y_d	$\Delta H@$
0.973	3.00	-1.80	1.0000	0.000	10.000	10.000	625.637	635.732	10.095	70.0	70.0	70.00	81.0	76.0	78.50	9.92	0.9943	1.7019
0.962	3.00	-1.80	1.0000	0.000	10.000	10.000	635.732	645.882	10.150	70.0	70.0	70.00	84.0	77.0	80.50	10.03	0.9926	1.7366
0.381	0.50	-1.10	1.0000	0.000	5.000	5.000	649.227	654.315	5.088	70.5	70.5	70.50	82.0	78.0	80.00	12.64	0.9962	1.8387
0.380	0.50	-1.10	1.0000	0.000	5.000	5.000	654.315	659.418	5.103	70.5	70.5	70.50	83.0	79.0	81.00	12.69	0.9952	1.8498
0.678	1.50	-1.40	1.0000	0.000	10.000	10.000	661.640	671.889	10.249	71.0	71.0	71.00	88.0	80.0	84.00	14.21	0.9923	1.7397
0.677	1.50	-1.40	1.0000	0.000	10.000	10.000	671.889	682.172	10.283	71.0	71.0	71.00	89.0	81.0	85.00	14.22	0.9908	1.7389
Averages																0.99357	1.76758	

Nomenclature	Equations
<p>P_b Barometric Pressure (in. Hg)</p> <p>Q Flow Rate (cfm)</p> <p>ΔH Orifice Pressure differential (in. H₂O)</p> <p>ΔP Inlet Pressure Differential (in. H₂O)</p> <p>V_d Gas Meter Volume - Dry (ft³)</p> <p>V_{ds} Standard Meter Volume - Dry (ft³)</p> <p>T_d Average Meter Box Temperature (°F)</p> <p>T_o Outlet Meter Box Temperature (°F)</p> <p>T_{ds} Average Standard Meter Temperature (°F)</p> <p>Y_d Meter Correction Factor (unitless), $Y_1 \leq Y_{avg} \pm 0.02$</p> <p>$Y_{ds}$ Standard Meter Correction Factor (unitless)</p> <p>$\Delta H@$ Orifice Pressure Differential giving 0.75 cfm of air at 68°F and 29.92 in. Hg (in. H₂O) $\Delta H@_1 \leq \Delta H@_{avg} \pm 0.2$</p> <p>$\Theta$ Duration of Run (minutes)</p>	$Y_d = (Y_{ds}) \left[\frac{V_{ds}}{V_d} \right] \left[\frac{T_d + 460}{T_{ds} + 460} \right] \left[\frac{P_b + \Delta P / 13.6}{P_b + \Delta H / 13.6} \right]$ $\Delta H@ = \frac{(0.0319)(\Delta H)}{P_b(T_o + 460)} \left[\frac{(T_{ds} + 460)\Theta}{(V_{ds})(Y_{ds})} \right]^2$ $Q = \frac{17.64(V_{ds})(P_b)}{(T_{ds} + 460)(\Theta)}$

Vacuum Gauge	
Standard (in.Hg)	Gauge (in.Hg)
4.7	5.0
9.9	10.0
14.9	15.0
20.2	20.0
24.5	25.0

Meter Box - Pyrometer Calibration Sheet

Meter Box No: 61-5 Office: _____
 Calibrated by: OLEG LAVROV Client: _____
 Date: 5/3/10 Job No: _____
 Temperature Scale Used: Fahrenheit Type of Calibration: Full-Test

Calibration Reference Settings (°F)	Pyrometer Reading for each Channel (°F)						
	1 Stack	2 Probe	3 Filter	4 Imp Out	5 Aux	6 DGM In	7 DGM Out
50	50	50	50				
100	100	99	100				
150	150	150	150				
200	200	200	200				
250	250	250	250				
300	300	300	300				
350	350	350	350				
400	400	400	400				
450	450	450	450				
500	500	499	500				
550	550	550	550				
600	600	600	600				

Tolerance = ±2°F difference from reference setting.

Calibration Reference Information

Reference Used: <u>Omega CL23A</u>	Serial No: <u>T-225950</u>
Calibrated By: <u>JH Metrology</u>	Exp. Date: <u>10/7/2010</u>
Calibration Report No: <u>RO44791</u>	

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Meter Box Critical Orifice Post-Test Calibration Data

Project No. 10955 Meter No. 61-5 Orifice C-3
 Location warehouse Meter Yd 0.9936 Orifice K' 0.4423
 Test Date 06/03/10 Meter ΔH@ 1.7676 Orifice Cal. Date 02/03/10
 Operator r. vicere Full Test Cal. Date 05/03/10

Leak Checks
 Negative Pressure Pass
No movement of manometer in one-minute
 Positive Pressure Pass
No movement of manometer in one-minute

Important: All leak checks must pass in order for calibration to be valid.

Barom. Press. (P_b) 29.03 in. Hg

Run	Elapsed Time (minutes)	Meter Volume (cc)	Meter Temperature		Ambient Temp. = T _a (°F)	Orifice ΔH (in. W.G.)	Vacuum (in. Hg)	Net Run Time = θ (minutes)	Net Meter Volume for Run = V _n (cc)	Avg Meter Temp. for Run T _m (°F)	DGM Calibration Factor = Y _i	Percent Variation = ΔY _i
			Inlet (°F)	Outlet (°F)								
	0.0	151.00	76	74								
1	5.0	153.92	76	74	76	1.00	21	5.0	2.92	75.0	0.9896	0.2%
2	10.0	156.85	76	74	78	1.00	21	5.0	2.93	75.0	0.9844	-0.3%
3	15.0	159.76	77	74	81	1.00	21	5.0	2.91	75.3	0.9889	0.1%
Average Y_i											0.9877	
Cal. Error											-0.6%	

Calculations and Specifications

$$Y_i = \frac{K' \times P_b \times (T_m + 460) \times \theta}{17.64 \times V_m \times (P_b + \frac{\Delta H}{13.6}) \times \sqrt{T_{amb} + 460}}$$

$$\Delta Y_i = \frac{Y_i - \bar{Y}_i}{\bar{Y}_i} \times 100 \quad \text{Spec.: } \Delta Y_i \leq \pm 2\%$$

$$\text{Cal. Error} = \frac{\bar{Y}_i - Y_d}{Y_d} \times 100 \quad \text{Spec.: } \text{Cal. Error} \leq \pm 5\%$$

D-7

Sample Probe Calibration

Probe Type: M5 with S-Type Pitot I.D. Number: 67-8-18
 Project Number: _____

Thermocouple Calibration

Reference Type: Thermocouple Reference I.D. No: 15-078-39 Pyrometer I.D. No: 80512890 Units: °F

Point No.	Target Temp.	Reference Temp.	Indicated Temp.	Temp. Difference	% Difference*	Specification
1	Ambient	70	70	0	0.00%	%Difference ≤ 1.5
2	200°F-250°F	218	217	1	0.15%	

* Based on Absolute Temperature (Rankine)

Does thermocouple assembly meet specifications? → YES

Pitot Tube Calibration (Wind Tunnel Method @ 49 ft/sec)

Reference Pitot I.D. No: Wind Tunnel Reference Pitot Cp: 0.99

Pitot Side 'A' :				Abs. Deviation from Avg. C _{P(A)} **	Specification Avg. C _p Deviations ≤ 0.01
Trial No.	Reference ΔP	Probe ΔP	Probe C _{P(S)} *		
1	0.549	0.812	0.814	0.003	
2	0.561	0.816	0.820	0.003	
3	0.556	0.815	0.818	0.000	
Side 'A' Average Probe C _{P(A)} =			0.8175	0.0021	

Pitot Side 'B' :				Abs. Deviation from Avg. C _{P(B)} **	Specification Avg. C _p Deviations ≤ 0.01
Trial No.	Reference ΔP	Probe ΔP	Probe C _{P(S)} *		
1	0.554	0.802	0.823	0.000	
2	0.555	0.803	0.823	0.000	
3	0.556	0.805	0.823	0.000	
Side 'B' Average Probe C _{P(B)} =			0.8228	0.0000	

'A' Average C _p 0.817	—	'B' Average C _p 0.823	=	Difference -0.006	Specification Difference ≤ 0.01
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Does assembly meet specifications? → YES

If "Yes", C_p = Average of Side 'A' and 'B' Cp values. If "No", Pitot must be replaced.

$$* C_{P(S)} = C_{P(STD)} \sqrt{\frac{\Delta p_{(STD)}}{\Delta p_{(S)}}}$$

$$** Deviation = |C_{P(S)} - \overline{C_{P(A \text{ or } B)}}|$$

All specifications are from EPA 600/9-76-008, section 3.1

Probe Cp= 0.820 Calibrated by: R ARNOLD Date: 03/04/2010

WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-5

FIELD DATA

E

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TEST LOCATION: FF Outlet

Mercury TESTING
FIELD DATA SHEET

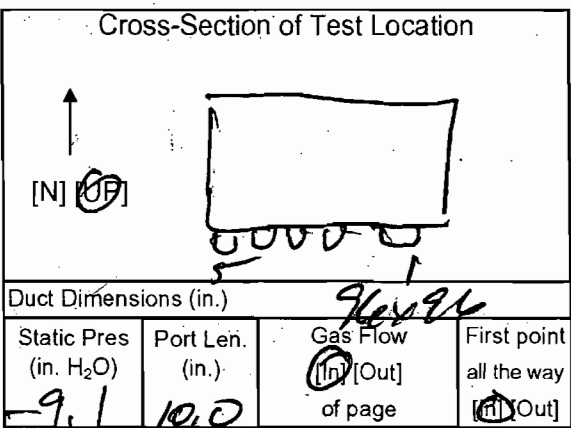
METHOD: 29 PAGE 1 OF 2

UNIT: 2 RUN: 1

Client <u>Wheelabrator</u>	Project No. <u>10911</u>
Plant <u>N. Brown</u>	Date <u>5/25/10</u>
Meter Operator <u>P. Bihner</u>	
Probe Operator <u>P. Bihner</u>	

Meter Box <u>61-5</u>	Sample Box No. <u>M10</u>
Meter Yd <u>0.9936</u>	Meter ΔH@ <u>6.7676</u>
K Factor <u>2.62</u>	Pitot Cp <u>0.82</u>

Leak Rate Before <u>0.002</u> (pm) [Lpm] @ <u>13</u> (in. Hg)
Leak Rate After <u>0.015</u> (pm) [Lpm] @ <u>10</u> (in. Hg)
Pitot Leak Check Before: <input checked="" type="checkbox"/> After: Good <input checked="" type="checkbox"/> Bad <input type="checkbox"/>



Amb. Temp. (°F) <u>80</u>	Bar. Press. <u>29.88</u> (in. Hg) [mbar]
Probe I.D. No. <u>878-18</u>	
Liner Material <u>Glass</u>	

Filter No. <u>N/A</u>	
Thimble No. <u>N/A</u>	
Nozzle Diameter <u>0.273</u>	Nozzle I.D. <u>2B-1</u>

Start Time: <u>7:39</u>	Stop Time: <u>9:50</u>
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E-3

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H ₂ O)	Orifice Setting ΔH (in. H ₂ O)	Gas Sample Volume V _m Init. Vol. (L)	Stack Temp. Ts (°F)	Probe T _p (°F)		Cond. Temp. T _c (°F)	DGM Inlet T _{min} (°F)	DGM Outlet T _{min} (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp T ₁ (°F)	Notes
						Set Points	Set Points						
				<u>909.450</u>		<u>280</u>	<u>280</u>						<u>O₂</u>
5-1	5	<u>0.58</u>	<u>1.5</u>	<u>913.02</u>	<u>312</u>	<u>248</u>	<u>280</u>	<u>65</u>	<u>79</u>	<u>80</u>	<u>6.0</u>	<u>N/A</u>	<u>10.2</u>
2	10	<u>0.52</u>	<u>1.4</u>	<u>916.37</u>	<u>312</u>	<u>246</u>	<u>283</u>	<u>61</u>	<u>81</u>	<u>80</u>	<u>5.5</u>		<u>9.6</u> <u>K22.68</u>
3	15	<u>0.45</u>	<u>1.2</u>	<u>919.49</u>	<u>310</u>	<u>252</u>	<u>283</u>	<u>62</u>	<u>84</u>	<u>80</u>	<u>5.5</u>		<u>10.1</u>
4	20	<u>0.44</u>	<u>1.2</u>	<u>922.67</u>	<u>311</u>	<u>257</u>	<u>247</u>	<u>63</u>	<u>87</u>	<u>81</u>	<u>5.5</u>		<u>8.8</u>
5	25	<u>0.42</u>	<u>1.1</u>	<u>925.650</u>	<u>309</u>	<u>250</u>	<u>248</u>	<u>64</u>	<u>89</u>	<u>81</u>	<u>5.0</u>		<u>9.8</u> <u>94.695</u>
4-1	30	<u>0.53</u>	<u>1.4</u>	<u>929.10</u>	<u>308</u>	<u>249</u>	<u>249</u>	<u>59</u>	<u>89</u>	<u>83</u>	<u>5.5</u>		<u>10.7</u> <u>(-0.045)</u>
2	35	<u>0.95</u>	<u>1.2</u>	<u>932.26</u>	<u>310</u>	<u>248</u>	<u>256</u>	<u>57</u>	<u>92</u>	<u>83</u>	<u>5.0</u>		<u>10.2</u>
3	40	<u>0.45</u>	<u>1.2</u>	<u>935.41</u>	<u>310</u>	<u>253</u>	<u>251</u>	<u>56</u>	<u>93</u>	<u>84</u>	<u>5.0</u>		<u>10.1</u>
4	45	<u>0.42</u>	<u>1.1</u>	<u>938.42</u>	<u>310</u>	<u>251</u>	<u>248</u>	<u>55</u>	<u>95</u>	<u>85</u>	<u>5.0</u>		<u>10.2</u>
5	50	<u>0.38</u>	<u>1.0</u>	<u>941.280</u>	<u>310</u>	<u>250</u>	<u>249</u>	<u>53</u>	<u>95</u>	<u>85</u>	<u>4.5</u>		<u>10.2</u> <u>94.335</u>
3-1	55	<u>0.45</u>	<u>1.2</u>	<u>944.52</u>	<u>308</u>	<u>249</u>	<u>246</u>	<u>60</u>	<u>94</u>	<u>86</u>	<u>5.0</u>		<u>10.6</u> <u>(-0.055)</u>
2	60	<u>0.52</u>	<u>1.4</u>	<u>947.95</u>	<u>311</u>	<u>250</u>	<u>254</u>	<u>61</u>	<u>95</u>	<u>86</u>	<u>5.5</u>		<u>10.1</u>
	Total												
	Average	<u>0.492</u>	<u>1.2804</u>	<u>81.368</u>	<u>309.240</u>				<u>89.3000</u>				

Sum of square roots. 14.9

Circle correct bracketed units on data sheet.

89.3000

QA/QC PB
Date 5/25/10



TEST LOCATION: FF Outlet

Mercury TESTING
FIELD DATA SHEET

METHOD: 29 PAGE 2 OF 2

UNIT: 2 RUN: 1

Client <u>Whitaker</u>	Project No. <u>109FF</u>
Plant <u>N. Brown</u>	Date <u>5/25/00</u>
Meter Operator <u>P. Bihun</u>	
Probe Operator <u>P. Bihun</u>	

Meter Box	Sample Box No.
Meter Y _d	Meter ΔH _@
K Factor	Pitot C _p
Leak Rate Before [cfm] [Lpm] @ (in. Hg)	
Leak Rate After [cfm] [Lpm] @ (in. Hg)	
Pitot Leak Check Before: <input type="checkbox"/> After: Good <input type="checkbox"/> Bad <input type="checkbox"/>	

Cross-Section of Test Location

↑
[N] [UP]

Duct Dimensions (in.)

Static Pres (in. H ₂ O)	Port Len. (in.)	Gas Flow [In] [Out] of page	First point all the way [In] [Out]
------------------------------------	-----------------	-----------------------------	------------------------------------

Amb. Temp. (°F)	Bar. Press. [in. Hg] [mbar]
Probe I.D. No.	
Liner Material	

Filter No.	
Thimble No.	
Nozzle Diameter	Nozzle I.D.

Start Time:	Stop Time:
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Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H ₂ O)	Orifice Setting ΔH (in. H ₂ O)	Gas Sample Volume V _m (L)	Stack Temp. T _s (°F)	Probe T _p (°F)	Filter T _f (°F)	Cond. Temp. T _c (°F)	DGM Inlet T _{min} (°F)	DGM Outlet T _{max} (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T ₁ (°F)	Notes
						Set Points							
						200	250						0.2
3	65	0.52	1.4	957.36	310	281	282	62	96	86	5.5	N/A	11.1
4	70	0.50	1.3	954.65	310	281	248	62	96	86	5.5		10.5
5	75	0.42	1.1	957.660	308	280	249	62	96	87	5.0		9.8
2-1	80	0.61	1.6	961.39	308	249	246	63	96	88	6.5		10.2 - 257.720
2	85	0.63	1.7	965.16	310	280	284	63	97	88	7.0		10.4 (-0.06)
3	90	0.44	1.2	968.39	308	252	251	62	97	88	5.5		10.4
4	95	0.52	1.4	971.85	309	251	249	63	96	88	6.0		9.4
5	100	0.57	1.5	975.45	309	280	248	60	97	88	6.0		9.9
1-1	105	0.33	0.88	978.15	305	249	248	60	95	88	4.5		10.2 (-0.06)
2	110	0.31	0.83	980.75	307	250	283	59	96	88	4.5		9.4
3	115	0.47	1.3	984.05	308	280	251	58	96	89	5.5		10.3
4	120	0.50	1.3	987.37	309	280	247	57	99	89	5.5		19.3
5	125	0.60	1.6	991.035	309	251	249	57	99	89	6.5		9.0
Total													
Average													

Sum of square roots.

Circle correct bracketed units on data sheet.



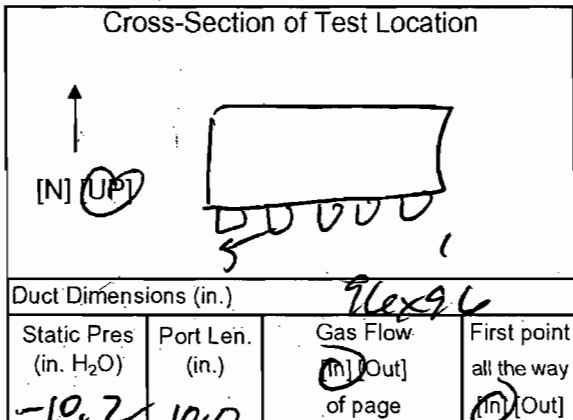
TEST LOCATION: FF Outlet
 UNIT: 2 RUN: 2

Mercury TESTING
 FIELD DATA SHEET

METHOD: 29 PAGE 1 OF 2

Client: Wheeler Project No.: 1025T
 Plant: N. Broward Date: 5/25/10
 Meter Operator: P. Bihary
 Probe Operator: P. Bihary

Meter Box: 61-15 Sample Box No.: 64 KP
 Meter Y_d: 0.9934 Meter ΔH_@: 1.7474
 K Factor: 2.64 Pitot C_p: 0.82
 Leak Rate Before: 0.003 [Lpm] @ 12 (in. Hg)
 Leak Rate After: 0.003 [Lpm] @ 11 (in. Hg)
 Pitot Leak Check Before: After: Good Bad



Amb. Temp. (°F): 84 Bar. Press.: 29.88 (in. Hg) [mbar]
 Probe I.D. No.: 678-18
 Liner Material: Glass

Filter No.: 2 1/4
 Thimble No.: 2 1/4
 Nozzle Diameter: 0.273 Nozzle I.D.: 273-1

Start Time: 10:18 Stop Time: 12:29

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H ₂ O)	Orifice Setting ΔH (in. H ₂ O)	Gas Sample Volume V _m (m ³ L)	Stack Temp. T _s (°F)	Probe T _p (°F)		Cond. Temp. T _c (°F)	DGM Inlet T _{m in} (°F)	DGM Outlet T _{m out} (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T _t (°F)	Notes
						Set Points	Set Points						
				<u>991.495</u>		<u>200</u>	<u>200</u>						<u>0.2</u>
<u>5-1</u>	<u>5</u>	<u>0.33</u>	<u>0.88</u>	<u>994.17</u>	<u>308</u>	<u>282</u>	<u>285</u>	<u>6.6</u>	<u>91</u>	<u>89</u>	<u>4.0</u>	<u>N/A</u>	<u>8.7</u>
<u>2</u>	<u>10</u>	<u>0.36</u>	<u>0.97</u>	<u>996.91</u>	<u>309</u>	<u>281</u>	<u>286</u>	<u>6.6</u>	<u>93</u>	<u>89</u>	<u>4.8</u>		<u>9.0</u>
<u>3</u>	<u>15</u>	<u>0.38</u>	<u>1.0</u>	<u>999.85</u>	<u>308</u>	<u>282</u>	<u>282</u>	<u>6.3</u>	<u>95</u>	<u>89</u>	<u>4.5</u>		<u>9.4</u>
<u>4</u>	<u>20</u>	<u>0.37</u>	<u>0.99</u>	<u>1002.71</u>	<u>309</u>	<u>281</u>	<u>281</u>	<u>6.1</u>	<u>98</u>	<u>89</u>	<u>4.5</u>		<u>9.0</u>
<u>5</u>	<u>25</u>	<u>0.35</u>	<u>0.94</u>	<u>1005.485</u>	<u>309</u>	<u>280</u>	<u>280</u>	<u>6.1</u>	<u>98</u>	<u>90</u>	<u>4.5</u>		<u>9.0</u>
<u>4+2</u>	<u>30</u>	<u>0.41</u>	<u>1.1</u>	<u>1008.48</u>	<u>308</u>	<u>248</u>	<u>281</u>	<u>6.3</u>	<u>97</u>	<u>90</u>	<u>5.0</u>		<u>9.5</u>
<u>2</u>	<u>35</u>	<u>0.45</u>	<u>1.2</u>	<u>1011.69</u>	<u>311</u>	<u>249</u>	<u>281</u>	<u>6.4</u>	<u>98</u>	<u>90</u>	<u>5.0</u>		<u>9.4</u>
<u>3</u>	<u>40</u>	<u>0.44</u>	<u>1.2</u>	<u>1014.91</u>	<u>310</u>	<u>282</u>	<u>281</u>	<u>6.4</u>	<u>100</u>	<u>91</u>	<u>5.1</u>		<u>9.8</u>
<u>4</u>	<u>45</u>	<u>0.50</u>	<u>1.3</u>	<u>1018.27</u>	<u>310</u>	<u>282</u>	<u>280</u>	<u>6.4</u>	<u>100</u>	<u>91</u>	<u>5.0</u>		<u>9.9</u>
<u>5</u>	<u>50</u>	<u>0.47</u>	<u>1.3</u>	<u>1021.425</u>	<u>310</u>	<u>280</u>	<u>280</u>	<u>6.4</u>	<u>101</u>	<u>91</u>	<u>5.0</u>		<u>9.9</u>
<u>3+1</u>	<u>55</u>	<u>0.46</u>	<u>1.2</u>	<u>1024.72</u>	<u>310</u>	<u>249</u>	<u>284</u>	<u>6.2</u>	<u>99</u>	<u>93</u>	<u>5.5</u>		<u>9.8</u>
<u>2</u>	<u>60</u>	<u>0.40</u>	<u>1.0</u>	<u>1027.61</u>	<u>309</u>	<u>249</u>	<u>280</u>	<u>5.8</u>	<u>100</u>	<u>93</u>	<u>5.0</u>		<u>9.7</u>
				<u>76.940</u>									
				<u>0.4585</u>									
				<u>1.1340</u>									
				<u>12.98</u>									
				<u>308.800</u>									
				<u>3711</u>									
				<u>95.7000</u>									
				<u>2255</u>									

Sum of square roots: 12.98

Circle correct bracketed units on data sheet.

95.7000

QA/QC: PR
 Date: 5/25/10



E-5

TEST LOCATION: FF Outlet

Mercury TESTING
FIELD DATA SHEET

METHOD: 29 PAGE 1 OF 2

UNIT: 2 RUN: 2

Client <u>Whitcomb</u>	Project No. <u>10911</u>
Plant <u>N. Broward</u>	Date <u>7/25/10</u>
Meter Operator <u>P. Bihun</u>	
Probe Operator <u>P. Bihun</u>	

Cross-Section of Test Location

↑
[N] [UP]

Duct Dimensions (in.)

Static Pres (in. H ₂ O)	Port Len. (in.)	Gas Flow [In] [Out] of page	First point all the way [In] [Out]
------------------------------------	-----------------	-----------------------------	------------------------------------

Amb. Temp. (°F)	Bar. Press. [in. Hg] [mbar]
Probe I.D. No.	
Liner Material	

Meter Box	Sample Box No.
Meter Y _d	Meter ΔH _@
K Factor	Pitot C _p
Leak Rate Before [cfm] [Lpm] @ (in. Hg)	
Leak Rate After [cfm] [Lpm] @ (in. Hg)	
Pitot Leak Check Before: <input type="checkbox"/> After: Good <input type="checkbox"/> Bad <input type="checkbox"/>	

Filter No.	
Thimble No.	
Nozzle Diameter	Nozzle I.D.

Start Time:	Stop Time:
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Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H ₂ O)	Orifice Setting ΔH (in. H ₂ O)	Gas Sample Volume V _m Init. Vol. [L]	Stack Temp. T _s (°F)	Probe T _p (°F)		Cond. Temp. T _c (°F)	DGM Inlet T _{min} (°F)	DGM Outlet T _{out} (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T _t (°F)	Notes
						Set Points	Set Points						
						280	280						O ₂
3	65	0.40	1.0	1030.45	310	281	280	57	99	92	5.0	N/A	8.2
4	70	0.45	1.2	1033.71	309	281	280	58	100	92	5.5		9.0
5	75	0.50	1.3	1037.045	310	280	280	58	101	92	6.0		9.6
2-1	80	0.49	1.3	1040.44	308	249	280	62	99	93	6.0		10.1
2	85	0.43	1.1	1043.42	309	249	281	62	101	93	5.5		9.1
3	90	0.48	1.2	1046.60	309	281	280	62	101	93	5.5		9.0
4	95	0.45	1.2	1049.76	308	281	280	63	102	94	5.5		8.0
5	100	0.55	1.4	1053.250	308	280	249	64	102	94	6.0		9.3
1-1	105	0.30	0.77	1055.79	307	249	284	64	99	95	4.5		9.2
2	110	0.35	0.90	1058.52	307	280	280	61	100	95	5.0		9.6
3	115	0.47	1.2	1061.74	308	280	249	58	102	95	6.0		9.0
4	120	0.56	1.4	1065.21	308	280	280	58	103	95	6.5		8.3
5	125	0.56	1.4	1068.670	308	281	280	58	103	95	6.5		8.4
Total													
Average													

Sum of square roots.

Circle correct bracketed units on data sheet.



E-6

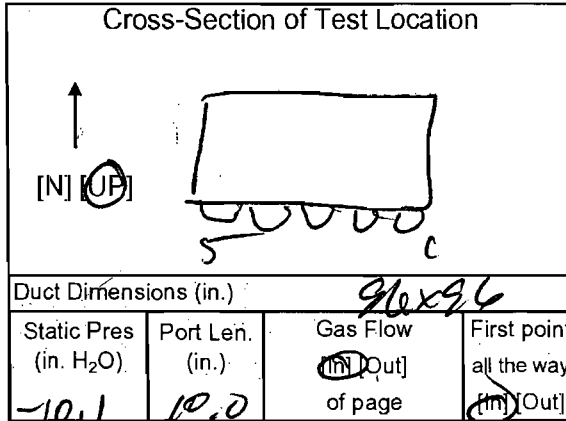
TEST LOCATION: FF Outlet
 UNIT: 2 RUN: 3

Mercury TESTING
FIELD DATA SHEET

METHOD: 29 PAGE 1 OF 2

Client <u>W. H. Johnson</u>	Project No. <u>1095F</u>
Plant <u>Pe. Brown</u>	Date <u>5/25/10</u>
Meter Operator <u>P. Schum</u>	
Probe Operator <u>P. Schum</u>	

Meter Box <u>41-F</u>	Sample Box No. <u>M10</u>
Meter Y_d <u>0.9936</u>	Meter ΔH <u>1.7676</u>
K Factor <u>2.57</u>	Pitot C_p <u>0.82</u>
Leak Rate Before <u>0.003</u> [Lpm] @ <u>12</u> (in. Hg)	
Leak Rate After <u>0.002</u> [Lpm] @ <u>10</u> (in. Hg)	
Pitot Leak Check Before: <input checked="" type="checkbox"/> After: Good <input checked="" type="checkbox"/> Bad <input type="checkbox"/>	



Amb. Temp. (°F) <u>81</u>	Bar. Press. <u>29.88</u> (in. Hg) (mbar)
Probe I.D. No. <u>107-8-18</u>	
Liner Material <u>Glass</u>	

Filter No. <u>N/A</u>	
Thimble No. <u>N/A</u>	
Nozzle Diameter <u>0.273</u>	Nozzle I.D. <u>273-1</u>

Start Time: <u>12:50</u>	Stop Time: <u>15:00</u>
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Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H ₂ O)	Orifice Setting ΔH (in. H ₂ O)	Gas Sample Volume V_m Init. Vol. (L)	Stack Temp. T_s (°F)	Probe T_p (°F)		Filter T_f (°F)	Cond. Temp. T_c (°F)	DGM Inlet T_{min} (°F)	DGM Outlet T_{mout} (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T_t (°F)	Notes
						Set Points	Set Points							
				<u>68.995</u>		<u>280</u>	<u>280</u>							<u>02</u>
5-1	5	<u>0.35</u>	<u>0.98</u>	<u>71.92</u>	<u>308</u>	<u>285</u>	<u>256</u>	<u>65</u>	<u>94</u>	<u>94</u>	<u>4.5</u>	<u>N/A</u>		<u>9.1</u>
2	10	<u>0.35</u>	<u>0.90</u>	<u>74.63</u>	<u>310</u>	<u>281</u>	<u>281</u>	<u>54</u>	<u>97</u>	<u>94</u>	<u>4.0</u>			<u>9.5</u>
3	15	<u>0.46</u>	<u>1.2</u>	<u>77.87</u>	<u>309</u>	<u>282</u>	<u>281</u>	<u>50</u>	<u>97</u>	<u>93</u>	<u>5.0</u>			<u>9.8</u>
4	20	<u>0.47</u>	<u>1.2</u>	<u>81.06</u>	<u>309</u>	<u>282</u>	<u>280</u>	<u>48</u>	<u>100</u>	<u>94</u>	<u>5.0</u>			<u>9.1</u>
5	25	<u>0.40</u>	<u>1.0</u>	<u>84.000</u>	<u>309</u>	<u>280</u>	<u>250</u>	<u>47</u>	<u>102</u>	<u>94</u>	<u>4.5</u>			<u>8.9</u>
4-1	30	<u>0.58</u>	<u>1.5</u>	<u>87.58</u>	<u>310</u>	<u>281</u>	<u>249</u>	<u>49</u>	<u>102</u>	<u>95</u>	<u>6.0</u>			<u>8.0</u>
2	35	<u>0.45</u>	<u>1.2</u>	<u>90.88</u>	<u>309</u>	<u>248</u>	<u>282</u>	<u>48</u>	<u>103</u>	<u>95</u>	<u>5.5</u>			<u>9.3</u>
3	40	<u>0.48</u>	<u>1.2</u>	<u>94.05</u>	<u>310</u>	<u>251</u>	<u>249</u>	<u>50</u>	<u>104</u>	<u>96</u>	<u>5.5</u>			<u>9.3</u>
4	45	<u>0.45</u>	<u>1.2</u>	<u>97.25</u>	<u>310</u>	<u>251</u>	<u>250</u>	<u>52</u>	<u>105</u>	<u>96</u>	<u>5.5</u>			<u>7.5</u>
5	50	<u>0.43</u>	<u>1.1</u>	<u>100.205</u>	<u>309</u>	<u>280</u>	<u>250</u>	<u>54</u>	<u>105</u>	<u>97</u>	<u>5.0</u>			<u>8.8</u>
3-1	55	<u>0.43</u>	<u>1.1</u>	<u>103.29</u>	<u>309</u>	<u>280</u>	<u>248</u>	<u>57</u>	<u>103</u>	<u>97</u>	<u>5.0</u>			<u>7.9</u>
2	60	<u>0.43</u>	<u>1.1</u>	<u>106.26</u>	<u>308</u>	<u>249</u>	<u>250</u>	<u>55</u>	<u>104</u>	<u>98</u>	<u>5.0</u>			<u>8.1</u>
Total				<u>78.975</u>										
Average		<u>0.476</u>	<u>1.192</u>		<u>308.740</u>				<u>100.1500</u>					

Sum of square roots.

Circle correct bracketed units on data sheet.



ORSAT READINGS

TEST LOCATION: EF Outlet

PAGE 1 OF 1

Client <u>Wheelabrator</u>	Project Number <u>10955</u>	$F_o = \frac{20.9 - \%O_2}{\%CO_2}$
Plant <u>N. Broward</u>	Unit <u>2</u>	
Orsat ID <u>6</u>	Fuel Type <u>waste</u>	Leak Check Passed <input checked="" type="checkbox"/>

Run Number	Method Number	Trial	Percent CO ₂	Percent O ₂ +CO ₂	Percent O ₂	F _o	Analyst	Analysis	
								Date	Time
1	29	1	9.5	18.6	9.1	1.24	C. Slomp	5/10/10	10:39
		2	9.6	18.5	9.9				
		3	9.6	18.6	9.0				
		Avg.	9.57		9.0				
2	29	1	9.8	18.8	9.0	1.21	C. Slomp	5/12/10	13:14
		2	9.8	18.8	9.0				
		3	9.8	18.8	9.0				
		Avg.	9.8		9.0				
3	29	1	9.8	18.8	9.0		C. Slomp	5/12/10	15:35
		2	9.7	18.8	9.0				
		3	9.8	18.8	9.0				
		Avg.	9.77		9.0				
		1							
		2							
		3							
		Avg.							
		1							
		2							
		3							
		Avg.							
		1							
		2							
		3							
		Avg.							

Repeat the analysis procedure until the results of any three analyses differ by no more than 0.2 percent by volume. Average the three acceptable values and report the results to the nearest 0.1 percent. Calculate F_o to verify results

Acceptable ranges for F_o :

Coal: Anthracite and Lignite	1.016-1.130	Gas: Natural	1.600-1.836
Bituminous	1.083-1.230	Propane	1.434-1.586
Oil: Distillate	1.260-1.413	Butane	1.405-1.553
Residual	1.210-1.370	Wood	1.000-1.120
Municipal Solid Waste	1.030-1.300	Wood Bark	1.003-1.130

Impinger Weight Sheet

Client <i>Wheelabrator</i>	Unit Name / Location <i>2 Stack FF Outlet</i>
Plant <i>N. Browns</i>	Job No. <i>10955</i> Method <i>29</i>

Run No. <i>1</i>	Filter Type <i>Quartz</i>	Sample Box No. <i>M10</i>
Date <i>5-25-10</i>	Lot No.	pH <i>-</i>
Analyst <i>C. Slimp</i>	Filter No. <i>-</i>	Rinse <i>+100ml H2O</i>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	Empty	<i>762.9</i>	<i>449.9</i>	<i>316.6</i>	
Impinger 2	100 ml 5%HNO3/10%H2O2	<i>692.3</i>	<i>529.2</i>	<i>123.1</i>	QA/QC <i>CS</i> Date <i>5-25-10</i>
Impinger 3	100 ml 5%HNO3/10%H2O2	<i>607.1</i>	<i>563.1</i>	<i>44.0</i>	
Impinger 4	Empty	<i>447.5</i>	<i>435.6</i>	<i>11.9</i>	
Impinger 5	100 ml 4%KMnO4/10%H2SO4	<i>530.9</i>	<i>527.7</i>	<i>2.8</i>	Total Weight (gm)
Impinger 6	100 ml 4%KMnO4/10%H2SO4	<i>538.0</i>	<i>537.7</i>	<i>0.3</i>	
Impinger 7	Silica Gel	<i>794.4</i>	<i>734.8</i>	<i>19.6</i>	<i>518.3</i>

Run No. <i>2</i>	Filter Type <i>Quartz</i>	Sample Box No. <i>68 KP</i>
Date <i>5-25-10</i>	Lot No.	pH <i>-</i>
Analyst <i>C. Slimp</i>	Filter No. <i>-</i>	Rinse <i>-</i>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	Empty	<i>792.4</i>	<i>437.4</i>	<i>319.0</i>	
Impinger 2	100 ml 5%HNO3/10%H2O2	<i>671.8</i>	<i>552.4</i>	<i>119.4</i>	QA/QC <i>CS</i> Date <i>5-25-10</i>
Impinger 3	100 ml 5%HNO3/10%H2O2	<i>550.4</i>	<i>530.6</i>	<i>19.8</i>	
Impinger 4	Empty	<i>440.6</i>	<i>437.8</i>	<i>2.8</i>	
Impinger 5	100 ml 4%KMnO4/10%H2SO4	<i>534.7</i>	<i>533.1</i>	<i>1.6</i>	Total Weight (gm)
Impinger 6	100 ml 4%KMnO4/10%H2SO4	<i>542.3</i>	<i>542.3</i>	<i>0</i>	
Impinger 7	Silica Gel	<i>765.3</i>	<i>750.2</i>	<i>15.1</i>	<i>473.7</i>

Run No. <i>3</i>	Filter Type	Sample Box No.
Date	Lot No.	pH
Analyst	Filter No.	Rinse

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	Empty	<i>822.1</i>	<i>446.3</i>	<i>373.8</i>	
Impinger 2	100 ml 5%HNO3/10%H2O2	<i>624.0</i>	<i>534.5</i>	<i>89.5</i>	QA/QC Date
Impinger 3	100 ml 5%HNO3/10%H2O2	<i>571.4</i>	<i>559.9</i>	<i>11.5</i>	
Impinger 4	Empty	<i>442.2</i>	<i>440.4</i>	<i>1.8</i>	
Impinger 5	100 ml 4%KMnO4/10%H2SO4	<i>528.7</i>	<i>526.8</i>	<i>1.9</i>	Total Weight (gm)
Impinger 6	100 ml 4%KMnO4/10%H2SO4	<i>543.5</i>	<i>543.6</i>	<i>-0.1</i>	
Impinger 7	Silica Gel	<i>718.9</i>	<i>702.7</i>	<i>16.2</i>	<i>494.6</i>

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WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-5

FIELD DATA PRINTOUTS

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Field Data Printout

Test Method: USEPA Method 29
Analyte: Mercury

Location: Unit 2 FF Outlet
 Test Run: 1
 Client: Wheelabrator North Broward, Inc.
 Project No: 10955
 Source Area (ft²): 64.00000
 Meter Operator: P. Bihun 505
 Probe Operator: P. Bihun 505
 Test Date: 5/25/10
 Start Time: 07:39
 Stop Time: 09:50
 Leak Rate Before: 0.002 cfm @ 13 "Hg
 Leak Rate After: 0.015 cfm @ 10 "Hg

Bar. Press. (in. Hg): 29.88
 Static P: -9.1
 O₂ (dry volume %): 9.03
 CO₂ (dry volume %): 9.57
 N₂+CO (dry volume %): 81.40

Nozzle ID No: 273-1
 Nozzle Diameter (D_n): 0.273
 Probe ID No: 67-8-18
 Pitot C_p: 0.8200
 Pitot Leak Check: Pass Fail

H₂O (condensate, ml or gm): 498.7
 H₂O (silica, g): 19.6
 Actual Moisture (%): 23.86

Meter Box ID. No: 61-5
 Meter ΔH@: 1.76776
 Meter Y_d: 0.99360

Traverse Point	Run Time 5.0 min/read	Pitot ΔP _s (in. H ₂ O)	Sample ΔH (in. H ₂ O)	Metered (dcf)	Stack T _e (°F)	Dry Gas Meter		√ΔP _s (calculated) (in. H ₂ O)	Volume (calculated) (ft³)	Isokinetics (calculated) (%)
						T _{m-in} (°F)	T _{m-out} (°F)			
	0.0			909.450						
5-01	5.0	0.58	1.50	913.020	312	79	80	0.76	3.57	106.4
5-02	10.0	0.52	1.40	916.370	312	81	80	0.72	3.35	105.2
5-03	15.0	0.45	1.20	919.490	310	84	80	0.67	3.12	104.9
5-04	20.0	0.44	1.20	922.670	311	87	81	0.66	3.18	107.8
5-05	25.0	0.42	1.10	925.650	309	89	81	0.65	2.98	103.0
LEAK CHECK	25.0			925.695						
4-01	30.0	0.53	1.40	929.100	308	89	83	0.73	3.40	104.6
4-02	35.0	0.45	1.20	932.260	310	92	83	0.67	3.16	105.1
4-03	40.0	0.45	1.20	935.410	310	93	84	0.67	3.15	104.6
4-04	45.0	0.42	1.10	938.420	310	95	85	0.65	3.01	103.2
4-05	50.0	0.38	1.00	941.280	310	95	85	0.62	2.86	103.0
LEAK CHECK	50.0			941.335						
3-01	55.0	0.45	1.20	944.520	308	94	86	0.67	3.18	105.3
3-02	60.0	0.52	1.40	947.950	311	95	86	0.72	3.43	105.7
3-03	65.0	0.52	1.40	951.360	310	96	86	0.72	3.41	104.9
3-04	70.0	0.50	1.30	954.650	310	96	86	0.71	3.29	103.2
3-05	75.0	0.42	1.10	957.660	308	96	87	0.65	3.01	102.7
LEAK CHECK	75.0			957.720						
2-01	80.0	0.61	1.60	961.390	308	96	88	0.78	3.67	104.0
2-02	85.0	0.63	1.70	965.160	310	97	88	0.79	3.77	105.2
2-03	90.0	0.44	1.20	968.390	308	97	88	0.66	3.23	107.6
2-04	95.0	0.52	1.40	971.850	309	96	88	0.72	3.46	106.2
2-05	100.0	0.57	1.50	975.415	309	97	88	0.75	3.56	104.4
LEAK CHECK	100.0			975.475						
2-01	105.0	0.33	0.88	978.150	305	95	88	0.57	2.67	102.8
2-02	110.0	0.31	0.83	980.750	307	96	88	0.56	2.60	103.1
2-03	115.0	0.47	1.30	984.050	308	96	89	0.69	3.30	106.3
2-04	120.0	0.50	1.30	987.370	309	99	89	0.71	3.32	103.5
2-05	125.0	0.60	1.60	991.035	309	99	89	0.77	3.66	104.4
Final	125.0		1.28040	81.36500	309.24000	89.30000		0.69120	81.36500	

25 points sampled
 QC: Check: Field Averages

Sq. Rt. ΔP	0.6912	1.2804	81.3650	309.2400	89.3000
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Avg. OK Avg. OK Avg. OK Avg. OK Avg. OK

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Field Data Printout

Test Method: USEPA Method 29
 Analyte: Mercury

Location: Unit 2 FF Outlet
 Test Run: 2
 Client: Wheelabrator North Broward, Inc.
 Project No: 10955
 Source Area (ff): 64.00000
 Meter Operator: P. Bihun 505
 Probe Operator: P. Bihun 505

Bar. Press. (in. Hg): 29.88
 Static P: -10.2
 O₂ (dry volume %): 9.00
 CO₂ (dry volume %): 9.80
 N₂+CO (dry volume %): 81.20

Nozzle ID No: 273-1
 Nozzle Diameter (D_n): 0.273
 Probe ID No: 67-B-18
 Pitot C_p: 0.8200
 Pitot Leak Check: Pass Fail

Test Date: 5/25/10
 Start Time: 10:18
 Stop Time: 12:29
 Leak Rate Before: 0.003 cfm @ 12 "Hg
 Leak Rate After: 0.003 cfm @ 11 "Hg

H₂O (condensate, ml or gm): 458.6
 H₂O (silica, g): 15.1
 Actual Moisture (%): 23.46

Meter Box ID. No: 61-5
 Meter ΔH@: 1.76776
 Meter Y_g: 0.99360

Traverse Point	Run Time 5.0 min/read	Pitot ΔP _s (in. H ₂ O)	Sample ΔH (in. H ₂ O)	Metered (dcf)	Stack T _s (°F)	Dry Gas Meter		√ΔP _s (calculated) (in. H ₂ O)	Volume (calculated) (ft ³)	Isokinetics (calculated) (%)
						T _{m-in} (°F)	T _{m-out} (°F)			
	0.0			991.495						
5-01	5.0	0.33	0.88	994.170	308	91	89	0.57	2.67	103.0
5-02	10.0	0.36	0.97	996.980	309	93	89	0.60	2.81	103.5
5-03	15.0	0.38	1.00	999.850	308	95	89	0.62	2.87	102.6
5-04	20.0	0.37	0.99	1002.710	309	98	89	0.61	2.86	103.4
5-05	25.0	0.35	0.94	1005.485	309	98	90	0.59	2.77	103.1
LEAK CHECK	25.0			1005.525						
4-01	30.0	0.41	1.10	1008.480	308	97	90	0.64	2.96	101.5
4-02	35.0	0.45	1.20	1011.690	311	98	90	0.67	3.21	105.4
4-03	40.0	0.44	1.20	1014.910	310	100	91	0.66	3.22	106.5
4-04	45.0	0.50	1.30	1018.270	310	100	91	0.71	3.36	104.3
4-05	50.0	0.47	1.20	1021.425	310	101	91	0.69	3.15	100.9
LEAK CHECK	50.0			1021.520						
3-01	55.0	0.46	1.20	1024.720	310	99	93	0.68	3.20	103.4
3-02	60.0	0.40	1.00	1027.610	309	100	93	0.63	2.89	100.0
3-03	65.0	0.40	1.00	1030.480	310	99	92	0.63	2.87	99.5
3-04	70.0	0.45	1.20	1033.710	309	100	92	0.67	3.23	105.5
3-05	75.0	0.50	1.30	1037.045	310	101	92	0.71	3.34	103.3
LEAK CHECK	75.0			1037.095						
2-01	80.0	0.49	1.30	1040.440	308	99	93	0.70	3.35	104.7
2-02	85.0	0.43	1.10	1043.420	309	101	93	0.66	2.98	99.4
2-03	90.0	0.48	1.20	1046.600	309	101	93	0.69	3.18	100.4
2-04	95.0	0.45	1.20	1049.760	308	102	94	0.67	3.16	102.8
2-05	100.0	0.55	1.40	1053.250	308	102	94	0.74	3.49	102.7
LEAK CHECK	100.0			1053.300						
1-01	105.0	0.30	0.77	1055.790	307	99	95	0.55	2.49	99.2
1-02	110.0	0.35	0.90	1058.520	307	100	95	0.59	2.73	100.6
1-03	115.0	0.47	1.20	1061.740	308	102	95	0.69	3.22	102.4
1-04	120.0	0.56	1.40	1065.210	308	103	95	0.75	3.47	101.0
1-05	125.0	0.56	1.40	1068.670	308	103	95	0.75	3.46	100.7
Final	125.0		1.13400	76.94000	308.80000	95.70000		0.65846	76.94000	

25 points sampled
 QC-Check: Field Averages
 Sq.Rt.ΔP: 0.6585 1.1340 76.9400 308.8000 95.7000
 Avg. OK Avg. OK Avg. OK Avg. OK Avg. OK

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Field Data Printout

Test Method: USEPA Method 29
 Analyte: Mercury

Location: Unit 2 FF Outlet
 Test Run: 3
 Client: Wheelabrator North Broward, Inc.
 Project No: 10955
 Source Area (ft²): 64.00000
 Meter Operator: P. Bihun 505
 Probe Operator: P. Bihun 505
 Test Date: 5/25/10
 Start Time: 12:50
 Stop Time: 15:00
 Leak Rate Before: 0.003 cfm @ 12 "Hg
 Leak Rate After: 0.002 cfm @ 10 "Hg

Bar. Press. (in. Hg): 29.88
 Static P: -10.1
 O₂ (dry volume %): 9.00
 CO₂ (dry volume %): 9.77
 N₂+CO (dry volume %): 81.23

Nozzle ID No: 273-1
 Nozzle Diameter (I_d): 0.273
 Probe ID No: 67-8-18
 Pitot C_p: 0.8200
 Pitot Leak Check: Pass Fail

H₂O (condensate, ml or gm): 478.4
 H₂O (silica, g): 16.2
 Actual Moisture (%): 23.92

Meter Box ID. No: 61-5
 Meter ΔH@: 1.76776
 Meter Y_d: 0.99360

Traverse Point	Run Time 5.0 min/read	Pitot ΔP _s (in. H ₂ O)	Sample ΔH (in. H ₂ O)	Metered (dcf)	Stack T _s (°F)	Dry Gas Meter		√ΔP _s (calculated) (√in. H ₂ O)	Volume (calculated) (ft ³)	Isokinetics (calculated) (%)
						T _{m-in} (°F)	T _{m-out} (°F)			
	0.0			68.995						
5-01	5.0	0.38	0.98	71.920	308	94	94	0.62	2.93	104.7
5-02	10.0	0.35	0.90	74.630	310	97	94	0.59	2.71	100.9
5-03	15.0	0.46	1.20	77.870	309	97	93	0.68	3.24	105.3
5-04	20.0	0.47	1.20	81.060	309	100	94	0.69	3.19	102.2
5-05	25.0	0.40	1.00	84.000	309	102	94	0.63	2.94	101.9
LEAK CHECK	25.0			84.040						
4-01	30.0	0.58	1.50	87.580	310	102	95	0.76	3.54	102.0
4-02	35.0	0.48	1.20	90.880	309	103	95	0.69	3.30	104.3
4-03	40.0	0.48	1.20	94.050	310	104	96	0.69	3.17	100.1
4-04	45.0	0.45	1.20	97.250	310	105	96	0.67	3.20	104.2
4-05	50.0	0.43	1.10	100.255	309	105	97	0.66	3.01	100.0
LEAK CHECK	50.0			100.295						
3-01	55.0	0.43	1.10	103.290	309	103	97	0.66	3.00	99.8
3-02	60.0	0.43	1.10	106.260	308	104	98	0.66	2.97	98.7
3-03	65.0	0.40	1.00	109.140	308	103	98	0.63	2.88	99.3
3-04	70.0	0.45	1.20	112.400	308	103	98	0.67	3.26	106.0
3-05	75.0	0.45	1.20	115.650	308	105	98	0.67	3.25	105.5
LEAK CHECK	75.0			115.695						
2-01	80.0	0.52	1.30	119.020	309	103	97	0.72	3.33	100.8
2-02	85.0	0.50	1.30	122.340	309	104	97	0.71	3.32	102.5
2-03	90.0	0.50	1.30	125.640	309	105	98	0.71	3.30	101.8
2-04	95.0	0.54	1.40	129.130	308	106	98	0.73	3.49	103.4
2-05	100.0	0.54	1.40	132.625	309	107	98	0.73	3.50	103.5
LEAK CHECK	100.0			132.670						
1-01	105.0	0.40	1.00	135.510	307	105	98	0.63	2.84	97.7
1-02	110.0	0.35	0.90	138.230	307	105	99	0.59	2.72	99.9
1-03	115.0	0.48	1.20	141.490	308	106	99	0.69	3.26	102.3
1-04	120.0	0.51	1.30	144.840	310	109	101	0.71	3.35	101.7
1-05	125.0	0.51	1.30	148.140	309	109	101	0.71	3.30	100.1
Final	125.0		1.17920	78.97500	308.76000	100.18000		0.67655	78.97500	

25 points sampled
 QC-Check: Field Averages Sq.Rt.ΔP 0.6766 1.1792 78.9750 308.7600 100.1800

Avg. OK Avg. OK Avg. OK Avg. OK Avg. OK

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USEPA Method 3 Laboratory Data

Location: Unit 2 FF Outlet
 Client: Wheelabrator North Broward, Inc.
 Project No: 10955
 Method: EPA Method 3
 Fuel Type: Municipal Waste
 F_o for Fuel: 1.03 to 1.3

Test Method: USEPA Method 29
Analyte: Mercury

Analyst: B. Wiltse
 Analyst Emp No: 561

Run Number	Trial	Percent CO ₂	Percent O ₂ +CO ₂	Percent O ₂	Percent N ₂	Dry Mol. Weight	F _o	Method of Analysis: Orsat
1	1	9.5	18.6	9.1	81.4	29.88	1.24042	<i>All measurements in spec.</i>
	2	9.6	18.5	8.9	81.5	29.89		
	3	9.6	18.6	9.1	81.3	29.90		
	Avg.	9.56667		9.03333	81.40000	29.89		
CEM or Other Avg:								<input checked="" type="checkbox"/> Fo value within expected range.

Run Number	Trial	Percent CO ₂	Percent O ₂ +CO ₂	Percent O ₂	Percent N ₂	Dry Mol. Weight	F _o	Method of Analysis: Orsat
2	1	9.8	18.8	9.0	81.2	29.93	1.21429	<i>All measurements in spec.</i>
	2	9.8	18.8	9.0	81.2	29.93		
	3	9.8	18.8	9.0	81.2	29.93		
	Avg.	9.80000		9.00000	81.20000	29.93		
CEM or Other Avg:								<input checked="" type="checkbox"/> Fo value within expected range.

Run Number	Trial	Percent CO ₂	Percent O ₂ +CO ₂	Percent O ₂	Percent N ₂	Dry Mol. Weight	F _o	Method of Analysis: Orsat
3	1	9.8	18.8	9.0	81.2	29.93	1.21843	<i>All measurements in spec.</i>
	2	9.7	18.7	9.0	81.3	29.91		
	3	9.8	18.8	9.0	81.2	29.93		
	Avg.	9.76667		9.00000	81.23333	29.92		
CEM or Other Avg:								<input checked="" type="checkbox"/> Fo value within expected range.

Run Number	Trial	Percent CO ₂	Percent O ₂ +CO ₂	Percent O ₂	Percent N ₂	Dry Mol. Weight	F _o	Method of Analysis:
	1							
	2							
	3							
	Avg.							
CEM or Other Avg:								<input type="checkbox"/> Fo value within expected range.

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USEPA Method 4 Laboratory Data

Location: Unit 2 FF Outlet
 Client: Wheelabrator North Broward, Inc.
 Project No: 10955

Test Method: USEPA Method 29
Analyte: Mercury
 Analyst: B. Wiltse
 Analyst Emp No: 561

Test Run: 1

	Contents	Gross (gm)	Tare (gm)	Net (gm)		
Impinger 1	Empty	762.5	445.9	316.6		
Impinger 2	5%HNO3/10%H2O2	652.3	529.2	123.1		
Impinger 3	5%HNO3/10%H2O2	607.1	563.1	44.0		
Impinger 4	Empty	447.5	435.6	11.9		
Impinger 5	4%KMnO4/10%H2SO4	530.5	527.7	2.8		
Impinger 6	4%KMnO4/10%H2SO4	538.0	537.7	0.3	498.7 Liquid (gm)	<i>Field Data Check</i>
Impinger 7	Silica Gel	754.4	734.8	19.6	0.0 less rinse (gm)	
Impinger 8					498.7 Net Liquid (gm)	<input checked="" type="checkbox"/> QA/QC OK
					+ 19.6 Silica Gel (gm)	<input checked="" type="checkbox"/> QA/QC OK
					518.3 Total Vlc (gm)	<input checked="" type="checkbox"/> QA/QC OK

Rinse: _____ (ml or gm)

Test Run: 2

	Contents	Gross (gm)	Tare (gm)	Net (gm)		
Impinger 1	Empty	752.4	437.4	315.0		
Impinger 2	5%HNO3/10%H2O2	671.8	552.4	119.4		
Impinger 3	5%HNO3/10%H2O2	550.4	530.6	19.8		
Impinger 4	Empty	440.6	437.8	2.8		
Impinger 5	4%KMnO4/10%H2SO4	534.7	533.1	1.6		
Impinger 6	4%KMnO4/10%H2SO4	542.3	542.3	0.0	458.6 Liquid (gm)	<i>Field Data Check</i>
Impinger 7	Silica Gel	765.3	750.2	15.1	0.0 less rinse (gm)	
Impinger 8					458.6 Net Liquid (gm)	<input checked="" type="checkbox"/> QA/QC OK
					+ 15.1 Silica Gel (gm)	<input checked="" type="checkbox"/> QA/QC OK
					473.7 Total Vlc (gm)	<input checked="" type="checkbox"/> QA/QC OK

Rinse: _____ (ml or gm)

Test Run: 3

	Contents	Gross (gm)	Tare (gm)	Net (gm)		
Impinger 1	Empty	822.1	448.3	373.8		
Impinger 2	5%HNO3/10%H2O2	624.0	534.5	89.5		
Impinger 3	5%HNO3/10%H2O2	571.4	559.9	11.5		
Impinger 4	Empty	442.2	440.4	1.8		
Impinger 5	4%KMnO4/10%H2SO4	528.7	528.8	1.9		
Impinger 6	4%KMnO4/10%H2SO4	543.5	543.6	-0.1	478.4 Liquid (gm)	<i>Field Data Check</i>
Impinger 7	Silica Gel	718.9	702.7	16.2	0.0 less rinse (gm)	
Impinger 8					478.4 Net Liquid (gm)	<input checked="" type="checkbox"/> QA/QC OK
					+ 16.2 Silica Gel (gm)	<input checked="" type="checkbox"/> QA/QC OK
					494.6 Total Vlc (gm)	<input checked="" type="checkbox"/> QA/QC OK

Rinse: _____ (ml or gm)

Test Run: _____

	Contents	Gross (gm)	Tare (gm)	Net (gm)		
Impinger 1	Empty					
Impinger 2	5%HNO3/10%H2O2					
Impinger 3	5%HNO3/10%H2O2					
Impinger 4	Empty					
Impinger 5	4%KMnO4/10%H2SO4					
Impinger 6	4%KMnO4/10%H2SO4					
Impinger 7	Silica Gel					
Impinger 8						

Rinse: _____ (ml or gm)

Liquid (gm)		<i>Field Data Check</i>
less rinse (gm)		
Net Liquid (gm)		<input type="checkbox"/> QA/QC OK
Silica Gel (gm)		<input type="checkbox"/> QA/QC OK
Total Vlc (gm)		<input type="checkbox"/> QA/QC OK

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WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-5

LABORATORY DATA

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Wheelabrator North Broward, Inc.
 Clean Air Project No: 10955
 Unit 2 FF Outlet

**USEPA Method 29
 Mercury (Hg) Laboratory Parameters**

Blank Analysis

m _{1b-B}	Fraction 1B Blank (µg)	<0.1000
m _{2b-B}	Fraction 2B Blank (µg)	<0.2000
m _{3a-B}	Fraction 3A Blank (µg)	<0.2000
m _{3b-B}	Fraction 3B Blank (µg)	<0.5000
m _{3c-B}	Fraction 3C Blank (µg)	<0.4000
m _{total-B}	Total Blank Amount (µg)	<1.4000

Run No.	1	2	3
Date (2010)	May 25	May 25	May 25
Start Time (approx.)	07:39	10:18	12:50
Stop Time (approx.)	09:50	12:29	15:00

Sample Analysis

m _{1b-S}	Fraction 1B Sample (µg)	0.1204	<0.1000	<0.1000
m _{2b-S}	Fraction 2B Sample (µg)	42.0524	20.5021	19.5846
m _{3a-S}	Fraction 3A Sample (µg)	<0.2000	<0.2000	<0.2000
m _{3b-S}	Fraction 3B Sample (µg)	<0.5000	<0.5000	<0.5000
m _{3c-S}	Fraction 3C Sample (µg)	0.8843	<0.4000	<0.4000
m _{total-S}	Total Sample Amount (µg)	43.0571	20.5021	19.5846

Allowable Blank

m _{T-B-allow}	Total Allowable Blank (µg)	0.0000	0.0000	0.0000
------------------------	----------------------------	--------	--------	--------

Sample Corrected for Blank

m _n	Total Sample Amount (µg)	43.0571	20.5021	19.5846
----------------	--------------------------	---------	---------	---------

Sample Corrected for Blank

m _{n-1b}	Fraction 1B (µg)	0.1204	<0.1000	<0.1000
m _{n-2b}	Fraction 2B (µg)	42.0524	20.5021	19.5846
m _{n-3a}	Fraction 3A (µg)	<0.2000	<0.2000	<0.2000
m _{n-3b}	Fraction 3B (µg)	<0.5000	<0.5000	<0.5000
m _{n-3c}	Fraction 3C (µg)	0.8843	<0.4000	<0.4000

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Clean Air Engineering, Inc.

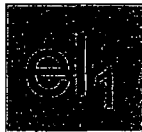
500 West Wood Street
Palatine, IL 60067

Project Number: 10955

Mercury

EPA Method 29 Analysis

Analytical Report
14553



Element One, Inc.

5022-C Wrightsville Av., Wilmington, NC 28403

910-793-0128 FAX: 910-792-6853 e1lab@e1lab.com

The following data for Analytical Report 14553
has been reviewed for completeness, accuracy,
adherence to method protocol,
and compliance with quality assurance guidelines.

Review by:

Ana White
June 8, 2010

Report Reviewed and Finalized By:

Ken Smith, Laboratory Director
June 8, 2010

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14553 CAE M29 Report Packet
Page 2 of 18

SUMMARY OF RESULTS

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14553 CAE M29 Report Packet
Page 3 of 18

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Summary of Analysis

Summary of Method 29 Mercury Analysis

Run Number	Average Total Catch, μg	Front half μg	H_2O_2 / HNO_3 μg	Empty Impinger μg	KMnO_4 μg	HCl μg
U2 FF Outlet R1 #1	43.1	0.122	42.2	< 0.2	< 0.5	0.889
#2		0.118	41.9	< 0.2	< 0.5	0.880
U2 FF Outlet R2 #1	20.5	< 0.1	20.5	< 0.2	< 0.5	< 0.4
#2		< 0.1	20.5	< 0.2	< 0.5	< 0.4
U2 FF Outlet R3 #1	19.6	< 0.1	19.5	< 0.2	< 0.5	< 0.4
#2		< 0.1	19.6	< 0.2	< 0.5	< 0.4
Field Blank #1	< 0.5	< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
#2		< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
Reagent Blank #1	< 0.5	< 0.1	< 0.2	< 0.2	< 0.5	< 0.4
#2		< 0.1	< 0.2	< 0.2	< 0.5	< 0.4

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14553 CAE M29 Report Packet

Page 4 of 18

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ANALYTICAL NARRATIVE

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14553 CAE M29 Report Packet

Page 5 of 18

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Element One Analytical Narrative

Client:	Clean Air, IL	Element One #:	14553
Client ID:	Wheelabrator North Broward	Analyst:	ESS
Method:	Method 29	Dates Received:	05/26/2010
Analytes:	Hg	Dates Analyzed:	06/02-04/2010

Summary of Analysis

Samples were analyzed for mercury on a PerkinElmer FIMS-100 CVAA mercury analyzer.

Detection Limits

The FIMS-100 CVAA instrument reporting limit for mercury was 0.004 µg per aliquot analyzed.

Analysis QA/QC

Duplicate analyses relative percent difference (RPD), spike sample recovery, and second source calibration verification data are summarized in the Quality Control Section. All QA/QC data was within the criteria of the method.

Additional Comments

The reported results have not been corrected for any blank or spike recovery values.

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QUALITY CONTROL SUMMARY

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14553 CAE M29 Report Packet
Page 7 of 18

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Summary of Quality Control Data

Mercury Duplicate Analysis RPD

(Method 29 QC limits: < %10 for RPD)

Run Number	Front half	H ₂ O ₂ /HNO ₃	Empty Imp	KMnO ₄	HCl
U2 FF Outlet R1	3.4%	0.6%	NA	NA	1.1%
U2 FF Outlet R2	NA	0.1%	NA	NA	NA
U2 FF Outlet R3	NA	0.6%	NA	NA	NA
Field Blank	NA	NA	NA	NA	NA
Reagent Blank	NA	NA	NA	NA	NA

Mercury Spike Recoveries

(Method 29 QC limits: ±25% for Spike Recoveries)

Run Number	Front half	H ₂ O ₂ /HNO ₄	Empty Imp	KMnO ₄	HCl
U2 FF Outlet R3 #1	98%	102%	82%	92%	115%
U2 FF Outlet R3 #2	108%	105%	83%	91%	113%

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14553 CAE M29 Report Packet

Page 8 of 18

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SAMPLE CUSTODY

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14553 CAE M29 Report Packet
Page 9 of 18

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CHAIN OF CUSTODY FORM

14553 201364

CLIENT <u>Wheelabrator</u>	PROJECT NO. <u>10955</u>	NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED	PAGE <u>1</u> OF <u>3</u>
PLANT <u>North Broward</u>	DEPT. <u>66</u>				REVISION NO. <u>1</u>
PROJECT MANAGER <u>Scott Brown</u>	RECOVERY PERSON: <u>Carl Slimp</u>				ADDITIONAL INFORMATION
JOB LEADER <u>Carl Slimp</u>					

CAE LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX	NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED	ADDITIONAL INFORMATION
	-	Lab	5-25-10	5% HNO ₃ / 10% H ₂ O ₂ Reagent Blank	1	200	✓	* Method 29
	1	Unit 2 FF Outlet	"	Imp-3 catch & Rinse	1	770	✓	
	2	"	"	"	1	744	✓	
	3	"	"	"	1	774	✓	
		Field Blank	"	"	1	300	✓	
		Reagent Blank Lab	5-25-10	I H ₂ O Blank	1	100	✓	

Relinquished by: (Signature) <u>Carl Slimp</u>	Date/Time <u>5/25/10</u>	Received by: (Signature)	Date/Time	Relinquished by: (Signature)	Date/Time
Courier:	Date/Time	Relinquished by: (Signature)	Date/Time	Rec'd for Analysis by: <u>Scott Brown</u>	Date/Time <u>5/26/10 0945</u>

Special Handling Instructions <u>Attn: Ken Smith</u>	This form was completed by: <u>Carl Slimp</u>	Clean Air Engineering 500 West Wood Street Palatine, IL 60067 800-627-0033 Fax (847) 991-3385 Samples received in good condition in Fisher brand containers. No empty container received
Forwarding Lab: <u>Element One</u>	Signature	
<u>5022-C Wrightsville Ave</u> <u>Wilmington, NC 28405</u>	Date <u>5/25/10</u>	
PO Number:		

CHAIN OF CUSTODY FORM

14553 201485

CLIENT <u>Wheelabrator</u>		PROJECT NO. <u>10955</u>		NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED			PAGE <u>2</u> OF <u>3</u>	
PLANT <u>North Broward</u>		DEPT. <u>66</u>				Metals*				REVISION NO. <u>1</u>
PROJECT MANAGER <u>Scott Brown</u>		RECOVERY PERSON: <u>Carl Slimp</u>								ADDITIONAL INFORMATION
JOB LEADER <u>Carl Slimp</u>										
CAE LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX						
-		Lab	5/25/10	Reagent Blank 47 RMM/101.42.304	2	100	✓		*Hg Method 29	
1		Unit 2 FF Outlet	5/25/10	Imp 5th catch & rinse	2	432	✓			
2		"	5/25/10	"	2	407	✓			
3		"	5/25/10	"	2	446	✓			
		Field Blank	5/25/10	"	2	400	✓			
-		Lab	5/25/10	D.I.W. Nitric acid Reagent						
1		Unit 2 FF Outlet	5/25/10	Imp 4 catch & Rinse	2	300	✓			
2		Unit 2 FF Outlet	"	"	2	105	✓			
3		"	"	"	2	105	✓			
FB 4		"	"	"	2	100	✓			
		1CS								
		2CS								
		3CS								
Relinquished by: (Signature)		Date/Time	Received by: (Signature)		Date/Time	Relinquished by: (Signature)		Date/Time		
<u>Carl Slimp</u>		5/25/10	<u>Carl Slimp</u>			<u>Scott Brown</u>		5/25/10 0945		
Courier:		Date/Time	Relinquished by: (Signature)		Date/Time	Req'd for Analysis by:		Date/Time		
Special Handling Instructions			This form was completed by:			Clean Air Engineering 500 West Wood Street Palatine, IL 60067 800-627-0033 Fax (847) 991-3385 DS-COC Palatine EXCL-F0-6716				
Attn: Ken Smith			<u>Carl Slimp</u>							
Forwarding Lab: <u>Element One</u> <u>5022-C Wrightsville Ave</u> <u>Wilmington, NC 28405</u>			Signature <u>Carl Slimp</u> Date <u>5-25-10</u>							
PO Number: <u>10955</u>										

CHAIN OF CUSTODY FORM

14553

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CLIENT <u>Wheelabrator</u>		PROJECT NO. <u>10955</u>		NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED			PAGE <u>3</u> OF <u>3</u>	
PLANT <u>North Broward</u>		DEPT. <u>66</u>				/ / / / /			REVISION NO. <u>1</u>	
PROJECT MANAGER <u>Scott Brown</u>		RECOVERY PERSON: <u>Carl Slimp</u>							ADDITIONAL INFORMATION	
JOB LEADER <u>Carl Slimp</u>										
CAE LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX						
	<u>Report Blank</u>	<u>Lab</u>	<u>5-25-10</u>	<u>Imp 506 8NHCl Rinse</u>	<u>1</u>	<u>225</u>	<u>1</u>			<u>Method 29</u>
	<u>1</u>	<u>Unit 2 FF Outlet</u>	<u>"</u>	<u>"</u>	<u>1</u>	<u>225</u>	<u>✓</u>			
	<u>2</u>	<u>"</u>	<u>"</u>	<u>"</u>	<u>1</u>	<u>225</u>	<u>✓</u>			
	<u>3</u>	<u>"</u>	<u>"</u>	<u>"</u>	<u>1</u>	<u>225</u>	<u>✓</u>			
	<u>Field Blank</u>	<u>"</u>	<u>"</u>	<u>"</u>	<u>1</u>	<u>225</u>	<u>✓</u>			
	<u>Report Blank</u>	<u>Lab</u>	<u>"</u>	<u>3 Quartz Filters</u>	<u>1</u>	<u>-</u>	<u>✓</u>			
	<u>1</u>	<u>Unit 2 FF Outlet</u>	<u>"</u>	<u>1 Quartz Filter</u>	<u>1</u>	<u>-</u>	<u>✓</u>			
	<u>2</u>	<u>"</u>	<u>"</u>	<u>"</u>	<u>1</u>	<u>-</u>	<u>✓</u>			
	<u>3</u>	<u>"</u>	<u>"</u>	<u>"</u>	<u>1</u>	<u>-</u>	<u>✓</u>			
	<u>Field Blank</u>	<u>"</u>	<u>"</u>	<u>"</u>	<u>1</u>	<u>-</u>	<u>✓</u>			
	<u>Report Blank</u>	<u>the Lab</u>	<u>"</u>	<u>0.2 L3</u>						
	<u>1</u>	<u>Unit 2 FF Outlet</u>	<u>"</u>	<u>1/2 Rinse w/ Nitric</u>	<u>1</u>	<u>100</u>	<u>✓</u>			
	<u>2</u>	<u>"</u>	<u>"</u>	<u>"</u>	<u>1</u>	<u>100</u>	<u>✓</u>			
	<u>3</u>	<u>"</u>	<u>"</u>	<u>"</u>	<u>1</u>	<u>100</u>	<u>✓</u>			
	<u>Field Blank</u>	<u>"</u>	<u>"</u>	<u>"</u>	<u>1</u>	<u>100</u>	<u>✓</u>			
Relinquished by: (Signature)		Date/Time	Received by: (Signature)		Date/Time	Relinquished by: (Signature)		Date/Time		
<u>Carl Slimp</u>		<u>5-25-10</u>								
Courier:		Date/Time	Relinquished by: (Signature)		Date/Time	Rec'd for Analysis by:		Date/Time		
						<u>Ken Brown</u>		<u>5/26/10 0945</u>		
Special Handling Instructions				This form was completed by:		Clean Air Engineering 500 West Wood Street Palatine, IL 60067 800-627-0033 Fax (847) 991-3385				
Attn: Ken Smith										
Forwarding Lab: <u>Element One</u> <u>5022-C Wrightsville Ave</u> <u>Wilmington, NC 28405</u>				Signature Date						
PO Number: <u>10955</u>						DS CQC Palatine EXCL-R0-97/96				

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ANALYTICAL DATA

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14553 CAE M29 Report Packet
Page 13 of 18

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Analytical Calculations

Mercury-

$$\text{Mercury Results } (\mu\text{g}) = \frac{\text{CVAA Results } (\mu\text{g}) * \text{Final Volume (ml)}}{\text{Aliquot (ml)}}$$

Where-

CVAA Results= Raw sample reading (μg)--*Hg-Data Sheet*

Aliquot= Sample Aliquot (Alq.)--*Hg-Data Sheet*

Final Volume=Final Volume (FV)*--*Sample Submission*

* With the exception of the BH fraction where-
=Received Volume (BV)--*Sample Submission*

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14553 CAE M29 Report Packet

Page 14 of 18

Analytical Calculations

Spike Recovery-

$$\text{Spike (\%)} = \frac{(\text{Spiked Result } (\mu\text{g/L}) - \text{Sample Result } (\mu\text{g/L}))}{\text{Spike Amount } (\mu\text{g/L})} \times 100$$

Where-

Spike Result = Raw sample concentration (ppb)--*ICP-Data Sheet*

Sample Result = Raw sample concentration (ppb)--*ICP-Data Sheet*

Spike Amount--*ICP-MS Spike Table*

Duplicate Analysis RPD-

$$\text{RPD (\%)} = \frac{(\text{Duplicate Result } (\mu\text{g/L}) - \text{Sample Result } (\mu\text{g/L}))}{\text{Average } (\mu\text{g/L})} \times 100$$

Where-

Sample Result and Duplicate Results=Raw sample concentration (ppb)--*ICP-Data Sheet*

$$\text{Average} = \frac{(\text{Duplicate} + \text{Sample Results})}{2}$$

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Method 29 Microwave Worksheet

14553-CAE J

Lab ID # e

Client:

Date Digested: 6/01/10 Initials: DV Worksheet Prepared by: DV

Auto Sample Loc.	Sample Lab ID	Sample Weight (g)	# of filters digested	Spike	Prep Volume (ml)	Weight In Micro / Weight Out Micro	Units	
1	LRB 14553				100			
2	14553-1		1		↓			
3	-2		1					
4	-3		1					
5	-4		1					
6	-5		1					
7	LRB 14567							
8	14567-1		1		↓			
9	-2		1					
10	-3		1					
11	-4		1					
12	LRB 14572							
13	14572-1		1					
14	-2		1		↓			
15	-3		1					
16	-4		1					
HNO ₃ lot # 1109090		6 ml						
HF lot # 5108120		2 ml						

Element One, Inc. Form 104 - Revision 1.0

PerkinElmer FIMS-100 CVA Mercury Analyzer

Sample_ID	Date	Time	Mean_Sig	Mean_Rd	Mean_Rt	Units	Alq.	Vol.	Sig 1	Reading-1	Result-1	Sig 2	Reading-2	Result-2
Calib Blank	6/2/2010	11:16:44	0.0002273			µg			0.0002273					
STD1=.004ug	6/2/2010	11:17:59	0.0013241			µg			0.0013241					
STD2=.04ug	6/2/2010	11:19:14	0.0123811			µg			0.0123811					
STD3=.08ug	6/2/2010	11:20:30	0.0255055			µg			0.0255055					
STD4=.16ug	6/2/2010	11:21:49	0.0486654			µg			0.0486654					
STD5=.2ug	6/2/2010	11:23:09	0.062729			µg			0.062729					
Reagent Blank	6/2/2010	11:24:56	0.0001649	0.0005306	0.0005306	µg			0.0001905	0.0006129	0.0006129	0.0001393	0.0004483	0.0004483
0.004ug = DL	6/2/2010	11:26:10	0.0013334	0.0042904	0.0042904	µg			0.0013334	0.0042904	0.0042904			
0.080ug = STD.2	6/2/2010	11:28:02	0.0266223	0.0856594	0.0856594	µg			0.0266223	0.0856594	0.0856594			
0.080ug = QC STD 3	6/2/2010	11:29:23	0.0253129	0.0814463	0.0814463	µg			0.0253129	0.0814463	0.0814463			
REAGENT BLANK	6/2/2010	11:30:40	0.0001304	0.0004197	0.0004197	µg			0.0001304	0.0004197	0.0004197			
0.004ug = DL	6/2/2010	12:38:38	0.0013526	0.0043519	0.0043519	µg	4	245	0.0013526	0.0043519	0.0043519			
0.080ug = STD.2	6/2/2010	12:39:54	0.0270315	0.086976	0.086976	µg	4	245	0.0270315	0.086976	0.086976			
REAGENT BLANK	6/2/2010	12:41:12	5.882E-05	0.0001893	0.0001893	µg	4	245	5.882E-05	0.0001893	0.0001893			
14553-2bh	6/2/2010	12:46:35	0.0358997	0.1155104	21.658191	µg	4	750	0.0365548	0.1176182	22.05341	0.0352446	0.1134025	21.262972
14553-2bh dup	6/2/2010	12:48:24	0.0339833	0.1093443	20.502058	µg	4	750	0.0340003	0.1093988	20.512277	0.0339664	0.1092898	20.49184
14553-3bh	6/2/2010	12:50:14	0.0316195	0.1017384	19.584649	µg	4	770	0.0315321	0.1014573	19.530533	0.0317069	0.1020196	19.638766
14553-3bh spk	6/2/2010	12:52:00	0.0573502	0.1845291	35.521845	µg	4	770	0.0570457	0.1835494	35.333259	0.0576547	0.1855087	35.710431
14553-4bh	6/2/2010	12:53:54	3.554E-05	0.0001144	0.0082912	µg	4	290	4.609E-05	0.0001483	0.0107525	2.499E-05	8.041E-05	0.0058299
14553-5bh	6/2/2010	12:55:45	0.0006076	0.0019551	0.0977538	µg	4	200	0.0006119	0.0019687	0.0984366	0.0006034	0.0019414	0.097071
0.004ug = DL	6/2/2010	13:00:36	0.001335	0.0042955	0.0042955	µg	4	540	0.001335	0.0042955	0.0042955			
0.080ug = STD.2	6/2/2010	13:01:53	0.0269307	0.0866518	0.0866518	µg	4	540	0.0269307	0.0866518	0.0866518			
REAGENT BLANK	6/2/2010	13:03:10	7.098E-05	0.0002284	0.0002284	µg	4	540	7.098E-05	0.0002284	0.0002284			
Calib Blank	6/2/2010	13:49:54	0.000316			µg	4	460	0.000316					
STD1=.004ug	6/2/2010	13:51:09	0.0013175			µg	4	460	0.0013175					
STD2=.04ug	6/2/2010	13:52:25	0.0129762			µg	4	460	0.0129762					
STD3=.08ug	6/2/2010	13:53:42	0.0256179			µg	4	460	0.0256179					
STD4=.16ug	6/2/2010	13:55:00	0.0469022			µg	4	460	0.0469022					
STD5=.2ug	6/2/2010	13:56:18	0.0598384			µg	4	460	0.0598384					
Reagent Blank	6/2/2010	13:58:07	4.445E-05	0.0001483	0.0001483	µg	4	460	5.793E-05	0.0001933	0.0001933	3.097E-05	0.0001034	0.0001034
0.004ug = DL	6/2/2010	13:59:21	0.001301	0.004341	0.004341	µg	4	460	0.001301	0.004341	0.004341			
0.080ug = STD.2	6/2/2010	14:00:38	0.0251842	0.0840349	0.0840349	µg	4	460	0.0251842	0.0840349	0.0840349			
REAGENT BLANK	6/2/2010	14:01:55	-0.0000003	-0.0000101	-0.0000101	µg	4	460	-0.0000003	-0.0000101	-0.0000101			
0.080ug = QC STD 3	6/2/2010	14:03:12	0.0254909	0.0850583	0.0850583	µg	4	460	0.0254909	0.0850583	0.0850583			
REAGENT BLANK	6/2/2010	14:04:29	-0.0000358	-0.0001196	-0.0001196	µg	4	460	-0.0000358	-0.0001196	-0.0001196			
0.004ug = DL	6/2/2010	14:46:20	0.0011737	0.0039163	0.0039163	µg	4	200	0.0011737	0.0039163	0.0039163			
0.080ug = STD.2	6/2/2010	14:47:37	0.0252917	0.0843937	0.0843937	µg	4	200	0.0252917	0.0843937	0.0843937			
REAGENT BLANK	6/2/2010	14:48:54	3.312E-05	0.0001105	0.0001105	µg	4	200	3.312E-05	0.0001105	0.0001105			
14553-1a	6/2/2010	15:06:54	0.0005986	0.0019974	0.0998712	µg	4	200	0.0005869	0.0019582	0.0979108	0.0006104	0.0020366	0.1018315
0.004ug = DL	6/2/2010	15:08:07	0.0011923	0.0039785	0.0039785	µg	4	200	0.0011923	0.0039785	0.0039785			
0.080ug = STD.2	6/2/2010	15:09:24	0.0238709	0.0796527	0.0796527	µg	4	200	0.0238709	0.0796527	0.0796527			
REAGENT BLANK	6/2/2010	15:10:41	-0.0000307	-0.0001024	-0.0001024	µg	4	200	-0.0000307	-0.0001024	-0.0001024			
14553-2a	6/2/2010	15:12:26	0.0001168	0.0003897	0.0194836	µg	4	200	0.0001068	0.0003565	0.0178243	0.0001267	0.0004229	0.0211428
14553-2a dup	6/2/2010	15:14:10	8.403E-05	0.0002804	0.0140196	µg	4	200	7.501E-05	0.0002503	0.0125162	9.304E-05	0.0003105	0.0155231
14553-3a	6/2/2010	15:15:55	0.0001782	0.0005945	0.0297255	µg	4	200	0.0001487	0.0004963	0.0248141	0.0002076	0.0006927	0.034637
14553-3a spk	6/2/2010	15:17:41	0.0197168	0.0657913	3.2895648	µg	4	200	0.0195507	0.0652369	3.2618446	0.019883	0.0663457	3.317285
14553-4a	6/2/2010	15:19:27	-0.0000558	-0.0001864	-0.0093248	µg	4	200	-0.0000393	-0.0001313	-0.0065663	-0.0000724	-0.0002416	-0.0120834
14553-5a	6/2/2010	15:21:13	-0.0000511	-0.0001705	-0.0085262	µg	4	200	-0.0000564	-0.0001883	-0.0094153	-0.0000457	-0.0001527	-0.0076371
0.004ug = DL	6/2/2010	15:29:38	0.0011039	0.0036836	0.0036836	µg	4	100	0.0011039	0.0036836	0.0036836			
0.080ug = STD.2	6/2/2010	15:30:55	0.0229953	0.076731	0.076731	µg	4	100	0.0229953	0.076731	0.076731			
REAGENT BLANK	6/2/2010	15:32:12	-0.0000291	-0.0000972	-0.0000972	µg	4	100	-0.0000291	-0.0000972	-0.0000972			
Calib Blank	6/2/2010	12:04:00	0.0003244			µg			0.0003244					
STD1=.004ug	6/2/2010	12:05:15	0.0010493			µg			0.0010493					
STD2=.04ug	6/2/2010	12:06:30	0.0114752			µg			0.0114752					
STD3=.08ug	6/2/2010	12:07:46	0.019871			µg			0.019871					
STD4=.16ug	6/2/2010	12:09:02	0.0451999			µg			0.0451999					
STD5=.2ug	6/2/2010	12:10:20	0.0538749			µg			0.0538749					
Reagent Blank	6/2/2010	12:12:05	4.13E-06	1.514E-05	1.514E-05	µg			-0.0000225	-0.0000826	-0.0000826	0.0000308	0.0001129	0.0001129
0.004ug = DL	6/2/2010	12:13:18	0.0010512	0.0038527	0.0038527	µg			0.0010512	0.0038527	0.0038527			
0.080ug = STD.2	6/2/2010	12:14:35	0.0215097	0.0788356	0.0788356	µg			0.0215097	0.0788356	0.0788356			
0.080ug = QC STD 3	6/2/2010	12:15:53	0.0214302	0.0785444	0.0785444	µg			0.0214302	0.0785444	0.0785444			
REAGENT BLANK	6/2/2010	12:17:10	-0.0000082	-0.0000301	-0.0000301	µg			-0.0000082	-0.0000301	-0.0000301			
0.004ug = DL	6/2/2010	14:23:45	0.0011029	0.0040424	0.0040424	µg	4	700	0.0011029	0.0040424	0.0040424			
0.080ug = STD.2	6/2/2010	14:25:02	0.0215955	0.07915	0.07915	µg	4	700	0.0215955	0.07915	0.07915			
REAGENT BLANK	6/2/2010	14:26:18	-0.0000341	-0.0001251	-0.0001251	µg	4	700	-0.0000341	-0.0001251	-0.0001251			
14553-1b	6/2/2010	14:44:00	0.0007574	0.0027761	0.3470089	µg	4	500	0.0000754	0.0027761	0.3470143	0.0007574	0.002776	0.3470034
0.004ug = DL	6/2/2010	14:45:12	0.0011372	0.0041679	0.0041679	µg	4	500	0.0011372	0.0041679	0.0041679			
0.080ug = STD.2	6/2/2010	14:46:28	0.022485	0.0824103	0.0824103	µg	4	500	0.022485	0.0824103	0.0824103			
REAGENT BLANK	6/2/2010	14:47:44	-0.0000325	-0.0001191	-0.0001191	µg	4	500	-0.0000325	-0.0001191	-0.0001191			
14553-2b	6/2/2010	14:49:27	0.0001569	0.000575	0.0718713	µg	4	500	0.0001505	0.0005515	0.0689422	0.0001633	0.0005984	0.0748004
14553-2b dup	6/2/2010	14:51:09	-0.0000292	-0.0001071	-0.0133894	µg	4	500	-0.0000393	-0.0001443	-0.0180379	-0.000019	-0.0000699	-0.008741
14553-3b	6/2/2010	14:52:51	-0.0000563	-0.0002065	-0.025816	µg	4	500	-0.0000444	-0.0001628	-0.0203532	-0.0000682	-0.0002502	-0.0312788
14553-3b spk	6/2/2010	14:54:33	0.019929	0.0730421	9.1302571	µg	4	500	0.0200039	0.0733169	9.1646105	0.019854	0.0727672	9.0959037
14553-4b	6/2/2010	14:56:17	-0.0000103	-0.000038	-0.004757	µg	4	500	1.083E-05	3.971E-05	0.0049642	-0.0000316	-0.0001158	-0.0144783
14553-5b	6/2/2010	14:58:01	-0.000101	-0.0003701	-0.046273	µg	4	500	-0.0000725	-0.0002659	-0.0332385	-0.0001294	-0.0004744	-0.0593075
0.004ug = DL	6/2/2010	15:09:06	0.0011778	0.0043167	0.0043167	µg	4	500	0.0011778	0.0043167	0.0043167			
0.080ug = STD.2	6/2/2010	15:10:22	0.0225533	0.0826607	0.0826607	µg	4	500	0.0225533	0.0826607	0.0826607			
REAGENT BLANK	6/2/2010	15:11:3												

PerkinElmer FIMS-100 CVA Mercury Analyzer

Sample_ID	Date	Time	Mean_Sig	Mean_Rd	Mean_Rt	Units	Alq.	Vol.	Sig 1	Reading-1	Result-1	Sig 2	Reading-2	Result-2
Calib Blank	6/3/2010	12:27:57	0.0003165			µg	40	1	0.0003165					
STD1=.004ug	6/3/2010	12:29:12	0.0010093			µg	40	1	0.0010093					
STD2=.04ug	6/3/2010	12:30:28	0.0106417			µg	40	1	0.0106417					
STD3=.08ug	6/3/2010	12:31:46	0.0258407			µg	40	1	0.0258407					
STD4=.16ug	6/3/2010	12:33:04	0.0476237			µg	40	1	0.0476237					
STD5=.2ug	6/3/2010	12:34:23	0.0567293			µg	40	1	0.0567293					
Reagent Blank	6/3/2010	12:36:11	6.156E-05	0.0002108	0.0002108	µg	40	1	0.0001238	0.0004238	0.0004238	-0.0000006	-0.0000021	-0.0000021
0.004ug = DL	6/3/2010	12:37:25	0.0011279	0.0038619	0.0038619	µg	40	1	0.0011279	0.0038619	0.0038619			
0.080ug = STD.2	6/3/2010	12:38:42	0.0240062	0.082198	0.082198	µg	40	1	0.0240062	0.082198	0.082198			
0.080ug = QC STD 3	6/3/2010	12:40:02	0.0246354	0.0843524	0.0843524	µg	40	1	0.0246354	0.0843524	0.0843524			
REAGENT BLANK	6/3/2010	12:41:19	0.0000087	0.0002979	0.0002979	µg	40	1	0.0000087	0.0002979	0.0002979			
0.004ug = DL	6/3/2010	13:45:23	0.0010489	0.0035915	0.0035915	µg	1	640	0.0010489	0.0035915	0.0035915			
0.080ug = STD.2	6/3/2010	13:46:40	0.0237285	0.0812469	0.0812469	µg	1	640	0.0237285	0.0812469	0.0812469			
REAGENT BLANK	6/3/2010	13:47:57	1.39E-06	4.78E-06	4.78E-06	µg	1	640	1.39E-06	4.78E-06	4.78E-06			
14553-1bh	6/3/2010	13:51:32	0.0127601	0.0436908	42.052412	µg	0.8	770	0.0127974	0.0438186	42.175395	0.0127227	0.043563	41.929428
0.004ug = DL	6/3/2010	14:08:48	0.0011625	0.0039805	0.0039805	µg	0.1	100	0.0011625	0.0039805	0.0039805			
0.080ug = STD.2	6/3/2010	14:10:05	0.0240042	0.082191	0.082191	µg	0.1	100	0.0240042	0.082191	0.082191			
REAGENT BLANK	6/3/2010	14:11:22	-0.0000021	-0.0000074	-0.0000074	µg	0.1	100	-0.0000021	-0.0000074	-0.0000074			
0.004ug = DL	6/3/2010	14:54:31	0.0012711	0.0043524	0.0043524	µg	0.1	100	0.0012711	0.0043524	0.0043524			
0.080ug = STD.2	6/3/2010	14:55:48	0.024692	0.084546	0.084546	µg	0.1	100	0.024692	0.084546	0.084546			
REAGENT BLANK	6/3/2010	14:57:05	2.048E-05	7.013E-05	7.013E-05	µg	0.1	100	2.048E-05	7.013E-05	7.013E-05			
14553-1fh	6/3/2010	15:00:39	0.0014066	0.0048162	0.1204042	µg	4	100	0.0014308	0.004899	0.1224741	0.0013824	0.0047334	0.1183343
14553-2fh	6/3/2010	15:02:27	0.001042	0.0035679	0.089197	µg	4	100	0.0010607	0.0036318	0.090794	0.0010234	0.003504	0.0876
14553-2fh dup	6/3/2010	15:04:15	0.0010216	0.0034979	0.0874483	µg	4	100	0.0010162	0.0034794	0.0869854	0.001027	0.0035164	0.0879111
14553-3fh	6/3/2010	15:06:03	0.0009289	0.0031806	0.0795155	µg	4	100	0.0009414	0.0032235	0.0805864	0.0009164	0.0031378	0.0784447
14553-3fh spk	6/3/2010	15:07:52	0.0241368	0.0826449	2.0661233	µg	4	100	0.022982	0.0786909	1.9672727	0.0252915	0.086599	2.1649738
14553-4fh	6/3/2010	15:09:41	-0.000135	-0.0004625	-0.0115641	µg	4	100	-0.0001193	-0.0004086	-0.010216	-0.0001508	-0.0005164	-0.0129121
14553-5fh	6/3/2010	15:11:31	-0.0000923	-0.0003162	-0.0079051	µg	4	100	-0.0000973	-0.0003331	-0.0083293	-0.0000873	-0.0002992	-0.0074808
0.004ug = DL	6/3/2010	15:17:35	0.0012434	0.0042574	0.0042574	µg	4	100	0.0012434	0.0042574	0.0042574			
0.080ug = STD.2	6/3/2010	15:18:52	0.0248084	0.0849447	0.0849447	µg	4	100	0.0248084	0.0849447	0.0849447			
REAGENT BLANK	6/3/2010	15:20:09	8.66E-06	2.967E-05	2.967E-05	µg	4	100	8.66E-06	2.967E-05	2.967E-05			
Calib Blank	6/4/2010	15:21:30	0.0002752			µg	4	400	0.0002752					
STD1=.004ug	6/4/2010	15:22:46	0.0011429			µg	4	400	0.0011429					
STD2=.04ug	6/4/2010	15:24:02	0.0129503			µg	4	400	0.0129503					
STD3=.08ug	6/4/2010	15:25:19	0.0250546			µg	4	400	0.0250546					
STD4=.16ug	6/4/2010	15:26:36	0.0488489			µg	4	400	0.0488489					
STD5=.2ug	6/4/2010	15:27:55	0.0551523			µg	4	400	0.0551523					
Reagent Blank	6/4/2010	15:29:44	0.0000635	0.000218	0.000218	µg	4	400	0.0000309	0.0001061	0.0001061	9.609E-05	0.00033	0.00033
0.004ug = DL	6/4/2010	15:30:57	0.0012291	0.0042201	0.0042201	µg	4	400	0.0012291	0.0042201	0.0042201			
0.080ug = STD.2	6/4/2010	15:32:14	0.02478	0.0850845	0.0850845	µg	4	400	0.02478	0.0850845	0.0850845			
0.080ug = QC STD 3	6/4/2010	15:36:19	0.0251713	0.0864282	0.0864282	µg	4	400	0.0251713	0.0864282	0.0864282			
REAGENT BLANK	6/4/2010	15:37:36	7.53E-06	2.587E-05	2.587E-05	µg	4	400	7.53E-06	2.587E-05	2.587E-05			
0.004ug = DL	6/4/2010	15:56:52	0.0012435	0.0042698	0.0042698	µg	4	400	0.0012435	0.0042698	0.0042698			
0.080ug = STD.2	6/4/2010	15:58:10	0.024999	0.0858364	0.0858364	µg	4	400	0.024999	0.0858364	0.0858364			
REAGENT BLANK	6/4/2010	15:59:27	1.989E-05	6.832E-05	6.832E-05	µg	4	400	1.989E-05	6.832E-05	6.832E-05			
14553-1c	6/4/2010	16:13:32	0.0025753	0.0088426	0.8842621	µg	4	400	0.0025888	0.0088891	0.8889055	0.0025618	0.0087962	0.8796187
14553-2c	6/4/2010	16:15:19	0.0003712	0.0012746	0.1274553	µg	4	400	0.0003733	0.0012818	0.1281819	0.0003691	0.0012673	0.1267288
14553-2c dup	6/4/2010	16:17:08	0.0004834	0.0016598	0.1659791	µg	4	400	0.0004747	0.0016301	0.1630086	0.000492	0.0016895	0.1689496
0.004ug = DL	6/4/2010	16:18:22	0.0012738	0.0043737	0.0043737	µg	4	400	0.0012738	0.0043737	0.0043737			
0.080ug = STD.2	6/4/2010	16:19:39	0.0242881	0.0833956	0.0833956	µg	4	400	0.0242881	0.0833956	0.0833956			
REAGENT BLANK	6/4/2010	16:20:57	3.279E-05	0.0001126	0.0001126	µg	4	400	3.279E-05	0.0001126	0.0001126			
14553-3c	6/4/2010	16:22:43	0.0004927	0.0016919	0.1691853	µg	4	400	0.0005317	0.0018257	0.1825665	0.0004538	0.001558	0.1558042
14553-3c spk	6/4/2010	16:24:33	0.0266467	0.0914941	9.149413	µg	4	400	0.0268816	0.0923006	9.230065	0.0264119	0.0906876	9.068761
14553-4c	6/4/2010	16:26:22	-0.0001329	-0.0004565	-0.0456574	µg	4	400	-0.0001588	-0.0005452	-0.0545283	-0.0001071	-0.0003678	-0.0367864
14553-5c	6/4/2010	16:28:09	2.089E-05	7.173E-05	0.0071734	µg	4	400	1.471E-05	5.052E-05	0.005053	2.706E-05	9.293E-05	0.0092938
0.004ug = DL	6/4/2010	16:29:21	0.0011815	0.0040567	0.0040567	µg	4	400	0.0011815	0.0040567	0.0040567			
0.080ug = QC STD 3	6/4/2010	16:31:58	0.0250831	0.0861251	0.0861251	µg	4	400	0.0250831	0.0861251	0.0861251			
REAGENT BLANK	6/4/2010	16:33:23	1.735E-05	0.0000596	0.0000596	µg	4	400	1.735E-05	0.0000596	0.0000596			

WHEELABRATOR NORTH BROWARD, INC.
POMPANO BEACH, FL

Client Reference No: Service Agreement
CleanAir Project No: 10955-5

PLANT DATA

H

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WHEELABRATOR NORTH BROWARD
TONS OF REFUSE PROCESSED PER STACK TEST RUN LOG

UNIT #2						
5/25/2010	Mercury	29	1	184.9	2.18	77.5
5/25/2010	Mercury	29	2	184.1	2.18	77.2
5/25/2010	Mercury	29	3	184.0	2.17	76.8

**Wheelabrator
NORTH BROWARD
Emission Test Log**

Date: 05/25/10
Start Time: 7:39:00
End Time: 9:50:00

	SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS	SPECIFIC GRAVITY
	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O	" H2O
Unit 1	537.26	319.45	46.99	38.30	8.69	12.27	304.31	6.66	-9.99	1.105
Unit 2 29 run 1	518.88	319.42	40.71	32.36	8.35	14.18	298.05	6.20	-10.14	1.105
Unit 3	438.89	319.68	33.09	28.71	4.38	17.44	308.11	6.25	-7.58	1.105

H - 4

	FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNGR CHEM FLOW	STEAM FLOW	AVAILABLE CaO
	KLBS/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBS/hr	
Unit 1	184.28	895.50	832.21	78.43	-0.10	273.82	1161.87	4.73	175.76	1.099
Unit 2	193.90	900.19	839.14	75.73	-0.10	271.61	1205.27	4.61	184.91	1.099
Unit 3	189.53	899.46	831.52	78.04	-0.09	280.16	1110.42	7.95	175.94	1.099

**Wheelabrator
NORTH BROWARD
Emission Test Log**

Date: 05/25/10
Start Time: 10:18:00
End Time: 12:29:00

	SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FEED OUT TEMP	FF DP	ID INLET PRESS	SPECIFIC GRAVITY	
	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O	" H2O	
Unit 1	524.94	319.76	40.54	32.43	8.10	13.95	302.55	6.53	-9.29	1.108	
Unit 2	29 run 2	512.08	319.99	36.87	30.45	6.42	15.32	297.22	6.06	-9.73	1.108
Unit 3		433.59	319.79	30.54	25.04	5.50	18.69	308.15	6.15	-7.21	1.108

H - 5

	FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	EGONO OUT TEMP	SH ROLL AVG	SNCR CHEM FLOW	STEAM FLOW	AVAILABLE CaO
	KLBs/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBs/hr	
Unit 1	183.44	895.43	831.16	73.74	-0.09	274.39	1170.74	5.19	175.23	1.126
Unit 2	191.71	899.83	830.32	73.51	-0.09	272.15	1174.63	7.06	184.14	1.126
Unit 3	188.76	899.21	825.69	74.28	-0.09	280.71	1129.83	10.27	175.60	1.126

**Wheelabrator
NORTH BROWARD
Emission Test Log**

Date: 05/25/10
Start Time: 12:50:00
End Time: 15:00:00

	SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS	SPECIFIC GRAVITY
	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O	" H2O
Unit 1	531.87	320.47	43.76	34.11	9.65	13.00	302.80	6.64	-9.51	1.107
Unit 2 29 run 3	513.16	320.13	37.33	29.99	7.34	15.24	296.53	6.21	-9.88	1.107
Unit 3	436.07	319.84	29.94	25.19	4.75	19.01	308.40	6.23	-7.20	1.107

	FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNCR CHEM FLOW	STEAM FLOW	AVAILABLE CaO
	KLBs/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBs/hr	
Unit 1	182.27	895.05	830.50	76.41	-0.10	274.13	1169.47	4.96	174.43	1.119
Unit 2	192.06	899.58	829.84	73.34	-0.09	271.92	1175.93	7.97	184.00	1.119
Unit 3	188.29	898.87	826.65	73.83	-0.09	280.48	1132.09	9.09	175.11	1.119

End of Appendix
H - 6