



**Wheelabrator North Broward Inc.**

A Waste Management Company

2600 N.W. 48th Street  
Pompano Beach, FL 33073  
(954) 971-8701  
(954) 971-8703 Fax

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AUG 07 2008

**BUREAU OF AIR REGULATION**

August 4, 2008

CERTIFIED MAIL #7005 1160 0002 3457 2160

Mr. Lee Hoefert  
Air Program Administrator  
Florida Department of Environmental Protection  
Southeast District  
400 North Congress Ave., Suite 200  
West Palm Beach, FL 33401

Re: Wheelabrator North Broward  
F.A.C. 62-296.416 Quarterly Mercury Stack Testing  
Second Quarter of 2008, Report Submittal

Dear Mr. Hoefert:

As required by F.A.C. 62-296.416, please find enclosed the 2008 second quarter report on mercury stack testing which was conducted on Unit #1.

I, the undersigned, am a responsible official, as defined in Rule 62-210.200, F.A.C., of the Title V source addressed in this submittal. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements and information in this document are true, accurate and complete.

If there are any questions, please contact this office at (954) 971-8701.

Sincerely,

Scott McIlvaine  
Plant Manager

cc: USEPA, Region IV, Pesticides and Toxics Management Division, Air & EPCRA Enforcement Branch, Air Enforcement Section CERTIFIED MAIL #7005 1160 0002 3457 2238  
**FDEP, Tallahassee, Bureau of Air Regulation, New Source Review Section,**  
CERTIFIED MAIL #7005 1160 0002 3457 2245  
Broward County Department of Planning and Environmental Protection, Air Quality Division  
CERTIFIED MAIL #7005 1160 0002 3457 2252

Chuck Faller (with)  
Tim Porter (without)  
Rob French - MPI - (with)  
Ram Tewari - BCWRS (without)  
File: 3.7.2 (without)  
5.1.3.2 (without)



**REPORT ON MERCURY TESTING**

**WHEELABRATOR NORTH BROWARD, INC.  
UNIT 1 FF OUTLET  
POMPANO BEACH, FL**

**CLIENT REFERENCE NO: 14800198  
CLEANAIR PROJECT NO: 10455-6  
REVISION 0: AUGUST 1, 2008**



Wheelabrator North Broward, Inc.  
2600 NW 48<sup>th</sup> Street  
Pompano Beach, FL 33073

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**REPORT ON MERCURY TESTING**

Performed for:  
**WHEELABRATOR NORTH BROWARD, INC.**  
**UNIT 1 FF OUTLET**  
**POMPANO BEACH, FL**

Client Reference No: 14800198  
CleanAir Project No: 10455-6  
Revision 0: August 1, 2008

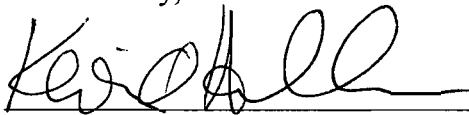
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To the best of our knowledge, the data presented in this report are accurate, complete, error free, legible and representative of the actual emissions during the test program.

Submitted by,

  
\_\_\_\_\_  
Scott Brown  
Project Manager  
sbrown@cleanair.com  
(800) 627-0033

Reviewed by,

  
\_\_\_\_\_  
Kevin O'Halloren  
Project Manager  
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**REVISION HISTORY**

**REPORT ON MERCURY TESTING**

Revision History

***DRAFT REPORT REVISION HISTORY***

<b>Revision:</b>	<b>Date</b>	<b>Pages</b>	<b>Comments</b>
D0a	07/23/08	All	Draft version of original document.

***FINAL REPORT REVISION HISTORY***

<b>Revision:</b>	<b>Date</b>	<b>Pages</b>	<b>Comments</b>
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**PROJECT OVERVIEW**

1-1

Wheelabrator North Broward, Inc. operates a Refuse to Energy Facility located in Pompano Beach, Florida. The facility's emission levels are regulated by the Florida Department of Environmental Protection. Wheelabrator North Broward, Inc. contracted Clean Air Engineering (CleanAir) to perform a compliance test program at their municipal waste combustor (MWC) facility in Pompano Beach, Florida. Testing was conducted in accordance with 40 CFR 60 Subpart Cb and applicable sections of PSD-FL-112(B) and PA86-22. The sampling was conducted at the Unit 1 Fabric Filter (FF) Outlet on June 27, 2008.

The testing included the determination of the following constituents:

- moisture (H<sub>2</sub>O);
- oxygen (O<sub>2</sub>);
- carbon dioxide (CO<sub>2</sub>);
- total flow (dscfm);
- mercury (Hg).

Coordinating and observing the field portion of the program were:

- |           |                                    |
|-----------|------------------------------------|
| C. Faller | - Wheelabrator North Broward, Inc. |
| E. Doak   | - CleanAir                         |

Chuck Faller of Wheelabrator North Broward Inc. provided all the process (operating) data. This data is presented in its entirety in Appendix H. The facility's process data (Bailey) time is 4 minutes ahead of their CEM time. CleanAir's test runs are all based on CEM time.

Table 1-1 outlines the schedule adhered to during the test program. Table 1-2 summarizes the results of the test program.

**Table 1-1:  
Schedule of Activities**

Run Number	Location	Method	Analyte	Date	Start Time	End Time
1	Unit 1 FF Outlet	USEPA Method 29	Trace Metals	06/27/08	09:01	11:17
2	Unit 1 FF Outlet	USEPA Method 29	Trace Metals	06/27/08	11:36	13:50
3	Unit 1 FF Outlet	USEPA Method 29	Trace Metals	06/27/08	14:10	16:30

**PROJECT OVERVIEW**

1-2

**Table 1-2:  
Summary of Test Results**

<u>Source</u> Constituent	Sampling Method	Average Emission	Permit Limit <sup>1</sup>
<u>Unit 1 FF Outlet</u> Mercury (µg/dscm @7% O <sub>2</sub> )	EPA M29	12	70

<sup>1</sup> Limits obtained from 40 Code of Federal Register part 60 Subpart Cb - Emission Guidelines and Compliance Times for Large Municipal Waste Combustors That Are Constructed on or Before September 20, 1994 published in Federal Register as 62 FR 45123 on December 19, 1995 as modified on August 25, 1997, 40 CFR 60.33b (a) (3), Rule 62-296.416 (3) (b) and and PSD-FL-112.

Due to delays, caused by equipment malfunction at South Broward, the North Broward scheduled test dates were pushed from June 26-27 to June 27-28. A copy of an e-mail notifying William Forrest of the FDEP of the loss of the first three test runs at South Broward is presented in Appendix I.

The test conditions and results of analysis are presented in Table 2-1 and the Quality Control and Quality Assurance Results are shown in Table 2-2 on page 2-2.

*End of Section 1 – Project Overview*

**RESULTS**

2-1

**Table 2-1:  
Unit 1 FF Outlet – Mercury**

Run No.	1	2	3	Average
Date (2008)	Jun 27	Jun 27	Jun 27	
Start Time (approx.)	09:01	11:36	14:10	
Stop Time (approx.)	11:17	13:50	16:30	
<b>Process Conditions</b>				
R <sub>p</sub> Steam Production Rate (Klbs/hour)	185	184	184	<b>184</b>
P <sub>1</sub> SDA Outlet Temperature (°F)	325	325	326	<b>325</b>
<b>Gas Conditions</b>				
O <sub>2</sub> Oxygen (dry volume %)	8.8	9.0	9.0	<b>8.9</b>
CO <sub>2</sub> Carbon dioxide (dry volume %)	10.6	10.4	10.2	<b>10.4</b>
T <sub>s</sub> Sample temperature (°F)	310	311	312	<b>311</b>
B <sub>w</sub> Actual water vapor in gas (% by volume)	23.5	22.9	22.4	<b>22.9</b>
<b>Gas Flow Rate</b>				
Q <sub>a</sub> Volumetric flow rate, actual (acfm)	184,949	190,696	194,736	<b>190,127</b>
Q <sub>std</sub> Volumetric flow rate, dry standard (dscfm)	94,895	98,560	101,207	<b>98,221</b>
<b>Sampling Data</b>				
V <sub>mstd</sub> Volume metered, standard (dscf)	70.31	72.37	73.55	<b>72.08</b>
%I Isokinetic sampling (%)	99.9	99.0	97.9	<b>98.9</b>
<b>Laboratory Data</b>				
m <sub>n-1b</sub> Fraction 1B Prorated (µg)	<0.1000	<0.1000	<0.1000	
m <sub>n-2b</sub> Fraction 2B Prorated (µg)	18.9204	21.3248	22.9907	
m <sub>n-3a</sub> Fraction 3A Prorated (µg)	<0.2000	<0.2000	<0.2000	
m <sub>n-3b</sub> Fraction 3B Prorated (µg)	<0.5000	<0.5000	<0.5000	
m <sub>n-3c</sub> Fraction 3C Prorated (µg)	<0.4000	<0.4000	<0.4000	
m <sub>n</sub> Total matter corrected for allowable blanks (µg)	18.9204	21.3248	22.9907	
<b>Mercury Results - Total</b>				
C <sub>sd</sub> Concentration (lb/dscf)	5.9E-10	6.5E-10	6.9E-10	<b>6.4E-10</b>
C <sub>sd7</sub> Concentration @7% O <sub>2</sub> (lb/dscf)	6.8E-10	7.6E-10	8.1E-10	<b>7.5E-10</b>
C <sub>sd</sub> Concentration (µg/dscm)	9.5	10.4	11.0	<b>10.3</b>
C <sub>sd7</sub> Concentration @7% O <sub>2</sub> (µg/dscm)	11	12	13	<b>12</b>
E <sub>lb/hr</sub> Rate (lb/hr)	0.0034	0.0038	0.0042	<b>0.0038</b>

8760  
x 1.0038

33,29 lbs/yr

29,78

TO

36.79 lbs/yr



**RESULTS**

2-2

**Table 2-2:  
Quality Assurance and Quality Control  
RPD RESULTS**

Run Number		FH Front half	BH H2O2/HNO4	A Empty Impinger	B KMnO4	C HCl
U1 FF Outlet N R1		NA	0.0%	NA	NA	NA
U1 FF Outlet N R2		NA	0.1%	NA	NA	NA
U1 FF Outlet N R3		NA	2.6%	NA	NA	NA
N Field Blank		NA	NA	NA	NA	NA
N Reagent Blank		NA	NA	NA	NA	NA
<b>Sample Spike and Recovery</b>						
U1 FF Outlet N R3	#1	108%	94%	97%	86%	91%
	#2	106%	94%	98%	86%	90%
<b>Blanks</b>						
N Field Blank	#1	< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
	#2	< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
N Reagent Blank	#1	< 0.1	< 0.2	< 0.2	< 0.5	< 0.4
	#2	< 0.1	< 0.2	< 0.2	< 0.5	< 0.4
<b>Meter Post Test Calibration Results = 1.3%</b>					<b>Limit = +/- 5%</b>	

End of Section 2 – Results

**DESCRIPTION OF INSTALLATION**

3-1

**PROCESS DESCRIPTION**

The North Broward Resource Recovery Facility operates three 750 tons per day municipal refuse fired, water wall boiler trains. The trains were manufactured by Babcock and Wilcox to produce electricity for sale to a local utility company. Each boiler is equipped a spray dryer absorber (SDA) for acid gas removal, followed by a fabric filter (FF) baghouse for the control of particulate emissions. Wheelabrator Air Pollution Control, Inc supplies the control equipment. Each fabric filter baghouse is followed by an induced draft fan, which directs the flue gas to a dedicated flue in a common stack.

Figure 3-1 shows a general schematic for the facility. The testing occurred at the Unit 1 FF Outlet as shown in Figure 3-2.

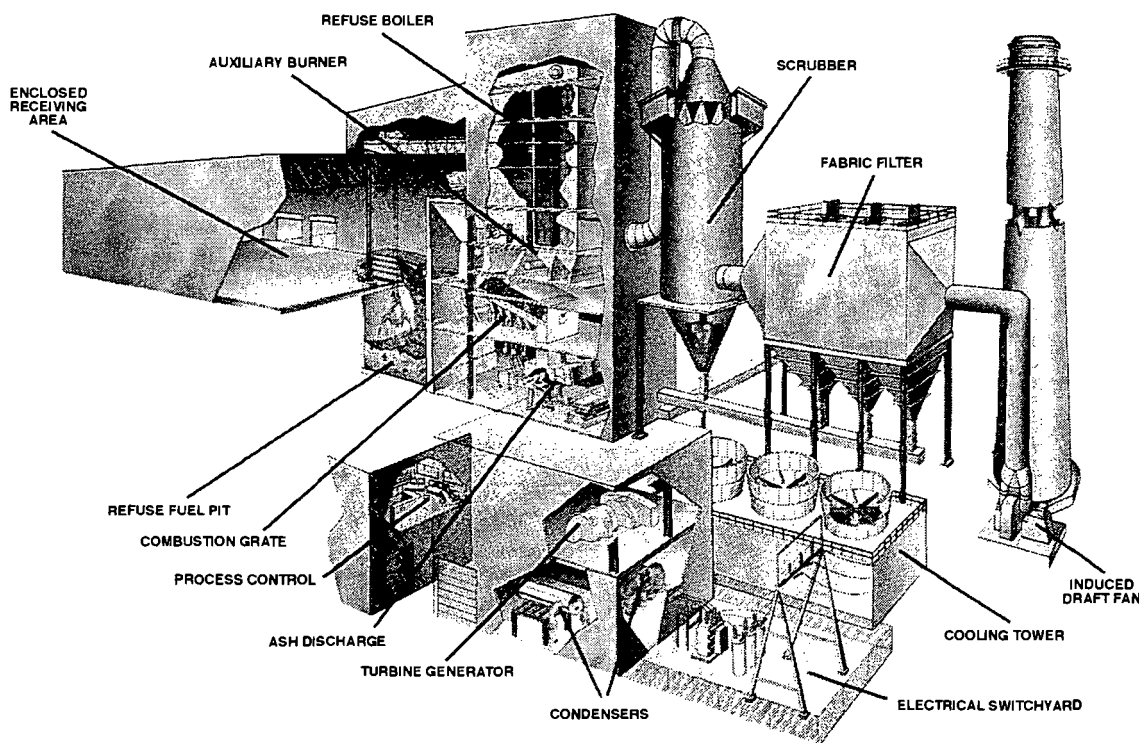


Figure 3-1: General Process Schematic

**DESCRIPTION OF INSTALLATION**

3-2

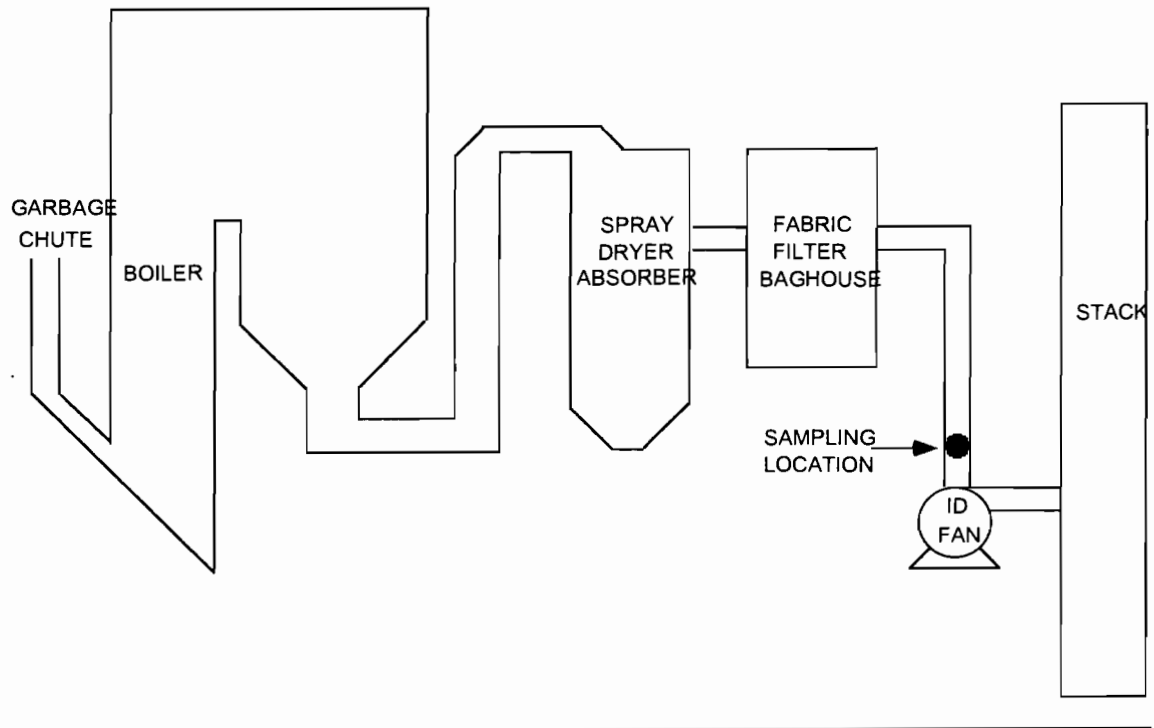


Figure 3-2: Process Schematic

**DESCRIPTION OF INSTALLATION**

3-3

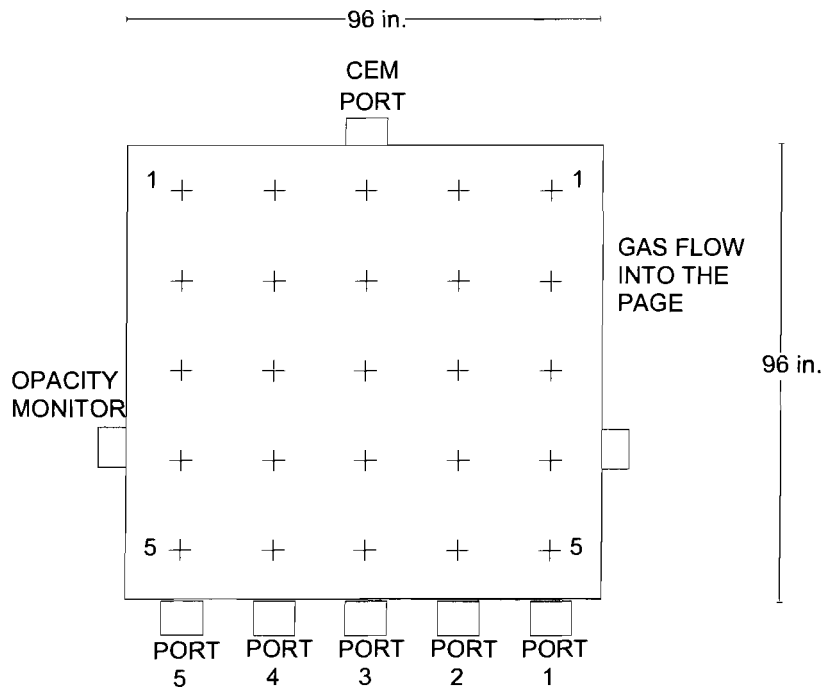
**DESCRIPTION OF SAMPLING LOCATION(S)**

Sampling point locations were determined according to EPA Method 1.

Table 3-1 outlines the sampling point configurations. Figure 3-3 illustrates the sampling points and orientation of sampling ports the source tested in the program.

**Table 3-1:  
Sampling Points**

Location	Constituent	Method	Run No.	Ports	Points per Port	Minutes per Point	Total Minutes	Figure
Unit 1 FF Outlet	Mercury	29	1-3	5	5	5	125	3-3



Sampling Point	Port to Point Distance (in.)
1	86.4
2	67.2
3	48.0
4	28.8
5	9.6

Equivalent Duct diameters upstream from flow disturbance (A): 0.5 Limit: 0.5  
Equivalent Duct diameters downstream from flow disturbance (B): 2.0 Limit: 2.0

**Figure 3-3: Unit 1 FF Outlet Sampling Point Determination (EPA Method 1)**

**METHODOLOGY**

Clean Air Engineering followed procedures as detailed in U.S. Environmental Protection Agency (EPA) Methods 1, 2, 3, 3B, 4 and 29. The following table summarizes the methods and their respective sources.

**Table 4-1:  
Summary of Sampling Procedures**

Title 40 CFR Part 60 Appendix A

Method 1	"Sample and Velocity Traverses for Stationary Sources"
Method 2	"Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)"
Method 3	"Gas Analysis for the Determination of Dry Molecular Weight"
Method 3B	"Gas Analysis for the Determination of Emission Rate Correction Factor or Excess Air"
Method 4	"Determination of Moisture Content in Stack Gases"
Method 29	"Determination of Metals Emissions from Stationary Sources"

These methods appear in detail in Title 40 of the Code of Federal Regulations (CFR) and on the World Wide Web at <http://www.cleanair.com>.

Diagrams of the sampling apparatus and major specifications of the sampling, recovery and analytical procedures are summarized for each method in Appendix A.

Clean Air Engineering followed specific quality assurance and quality control (QA/QC) procedures as outlined in the individual methods and in USEPA "Quality Assurance Handbook for Air Pollution Measurement Systems: Volume III Stationary Source-Specific Methods", EPA/600/R-94/038C. Additional QA/QC methods as prescribed in Clean Air's internal Quality Manual were also followed. Results of all QA/QC activities performed by Clean Air Engineering are summarized in Appendix D.

*End of Section 4 – Methodology*

WHEELABRATOR NORTH BROWARD, INC.  
POMPANO BEACH, FL

Client Reference No: 14800198  
CleanAir Project No: 10455-6

**APPENDIX**

**5-1**

TEST METHOD SPECIFICATIONS.....	A
SAMPLE CALCULATIONS.....	B
PARAMETERS.....	C
QA/QC DATA.....	D
FIELD DATA.....	E
FIELD DATA PRINTOUTS.....	F
LABORATORY DATA.....	G
PLANT DATA.....	H
PERTINENT CORRESPONDENCE.....	I

WHEELABRATOR NORTH BROWARD, INC.  
POMPANO BEACH, FL

Client Reference No: 14800198  
CleanAir Project No: 10455-6

**TEST METHOD SPECIFICATIONS**

A

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## Specification Sheet for

## EPA Method 29

Source Location Name(s) Unit 1 FF Outlet  
 Pollutant(s) to be Determined Mercury  
 Other Parameters to be Determined from Train Gas Density, Moisture, Flow Rate

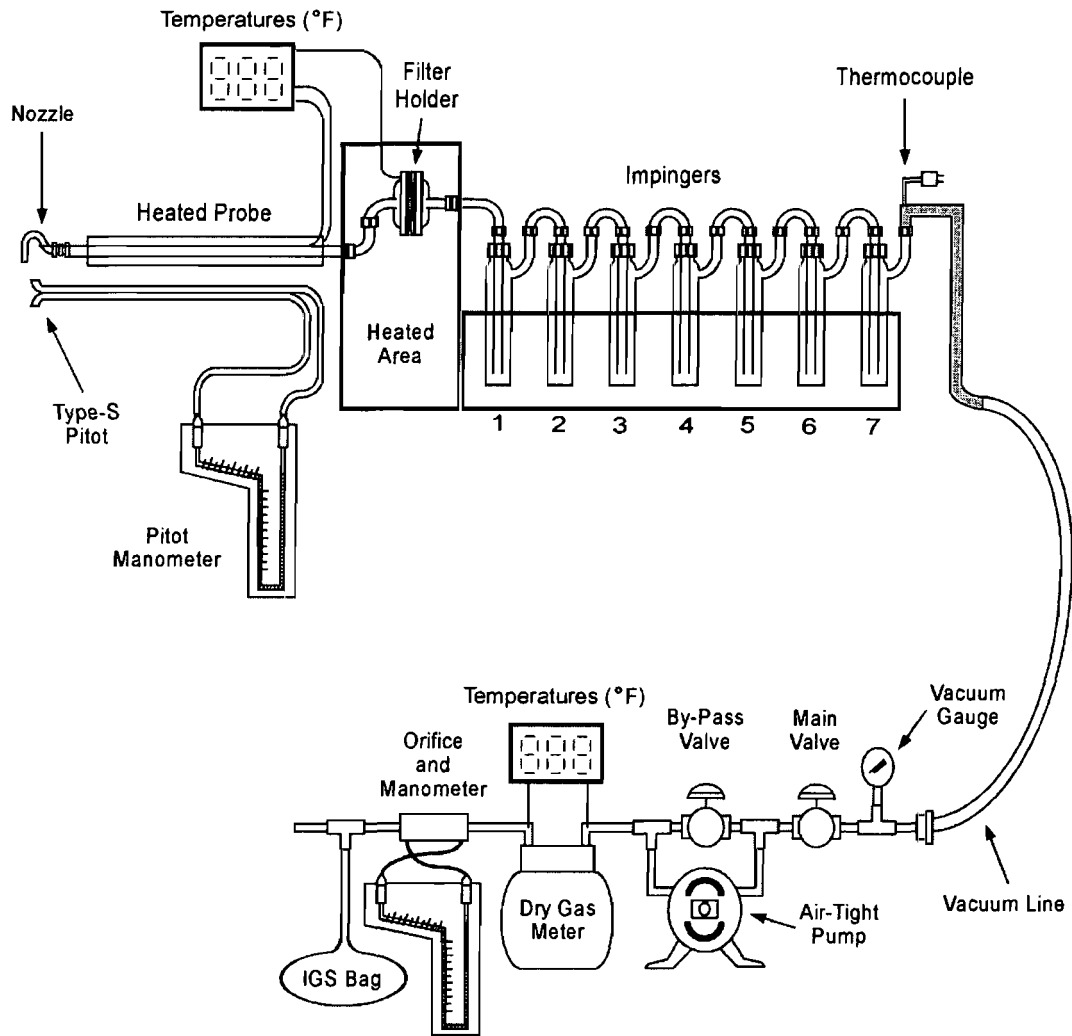
	<b>Standard Method Specification</b>	<b>Actual Specification Used</b>
<b>Pollutant Sampling Information</b>		
Duration of Run	N/A	125 minutes
No. of Sample Traverse Points	N/A	25
Sample Time per Point	N/A	5 minutes
Sampling Rate	Isokinetic (90-110%)	Isokinetic (90-110%)
<b>Sampling Probe</b>		
Nozzle Material	Borosilicate or Quartz Glass	Borosilicate Glass
Nozzle Design	Button-Hook or Elbow	Button-Hook
Probe Liner Material	Borosilicate or Quartz Glass	Borosilicate Glass
Effective Probe Length	N/A	8 feet
Probe Temperature Set-Point	248°F±25°F	248°F±25°F
<b>Velocity Measuring Equipment</b>		
Pitot Tube Design	Type S	Type S
Pitot Tube Coefficient	N/A	0.84
Pitot Tube Calibration by	Geometric or Wind Tunnel	Geometric
Pitot Tube Attachment	Attached to Probe	Attached to Probe
<b>Metering System Console</b>		
Meter Type	Dry Gas Meter	Dry Gas Meter
Meter Accuracy	±2%	±1%
Meter Resolution	N/A	0.01 cubic feet
Meter Size	N/A	0.1 dcf/revolution
Meter Calibrated Against	Wet Test Meter or Standard DGM	Wet Test Meter
Pump Type	N/A	Rotary Vane
Temperature Measurements	N/A	Type K Thermocouple/Pyrometer
Temperature Resolution	5.4°F	1.0°F
ΔP Differential Pressure Gauge	Inclined Manometer or Equivalent	Inclined Manometer
ΔH Differential Pressure Gauge	Inclined Manometer or Equivalent	Inclined Manometer
Barometer	Mercury or Aneroid	Digital Barometer calibrated w/Mercury Aneroid
<b>Filter Description</b>		
Filter Location	After Probe	Exit of Probe
Filter Holder Material	Borosilicate Glass	Borosilicate Glass
Filter Support Material	Teflon (or other non-metallic)	Teflon
Cyclone Material	N/A	None
Filter Heater Set-Point	248°F±25°F	248°F±25°F
Filter Material	Quartz or Glass Fiber	Quartz Fiber
<b>Other Components</b>		
Description	N/A	N/A
Location	N/A	N/A
Operating Temperature	N/A	N/A

## Specification Sheet for

## EPA Method 29

	<b>Standard Method Specification</b>	<b>Actual Specification Used</b>
<b>Impinger Train Description</b>		
Type of Glassware Connections	Ground Glass or Equivalent	Screw Joint with Silicone Gasket
Connection to Probe or Filter by	Direct Glass Connection	Direct Glass Connection
Number of Impingers	7	7
<b>Impinger Stem Types</b>		
Impinger 1	Modified Greenburg-Smith	Modified Greenburg-Smith
Impinger 2	Modified Greenburg-Smith	Modified Greenburg-Smith
Impinger 3	Greenburg-Smith	Greenburg-Smith
Impinger 4	Modified Greenburg-Smith	Modified Greenburg-Smith
Impinger 5	Modified Greenburg-Smith	Modified Greenburg-Smith
Impinger 6	Modified Greenburg-Smith	Modified Greenburg-Smith
Impinger 7	Modified Greenburg-Smith	Modified Greenburg-Smith
Impinger 8	Modified Greenburg-Smith	Modified Greenburg-Smith
<b>Gas Density Determination</b>		
Sample Collection	Multi-point integrated	Multi-Point Integrated
Sample Collection Medium	Flexible Gas Bag	Vinyl Bag
Sample Analysis	Orsat or Fyrite Analyzer	Orsat
<b>Sample Recovery Information</b>		
Probe Brush Material	Non-metallic swab or bristle	Teflon Mat
Probe Rinse Reagent	0.1N Nitric Acid	0.1 N Nitric Acid
Probe Rinse Wash Bottle Material	Glass or Teflon	Teflon
Probe Rinse Storage Container	Polyethylene or glass	Polyethylene
Filter Recovered?	Yes	Yes
Filter Storage Container	Petri Dish - Glass or Polystyrene	Polyethylene
Impinger Contents Recovered?	Yes	Yes
Impinger Rinse Reagent	See Method 29 Recovery Flow Chart	See Recovery Flow Chart
Impinger Wash Bottle	Glass or Teflon	Teflon
Impinger Storage Container	See Recovery Flow Chart	See Recovery Flow Chart
<b>Analytical Information</b>		
Method 4 H <sub>2</sub> O Determination by	Volumetric or Gravimetric	Gravimetric and Volumetric
Filter Preparation Conditions	See Method 29 Analytical Flow Chart	For Metals Analysis
Front-Half Rinse Preparation	See Method 29 Analytical Flow Chart	See Analytical Flow Chart
Back-Half Analysis	See Method 29 Analytical Flow Chart	See Analytical Flow Chart
Additional Analysis	None	None

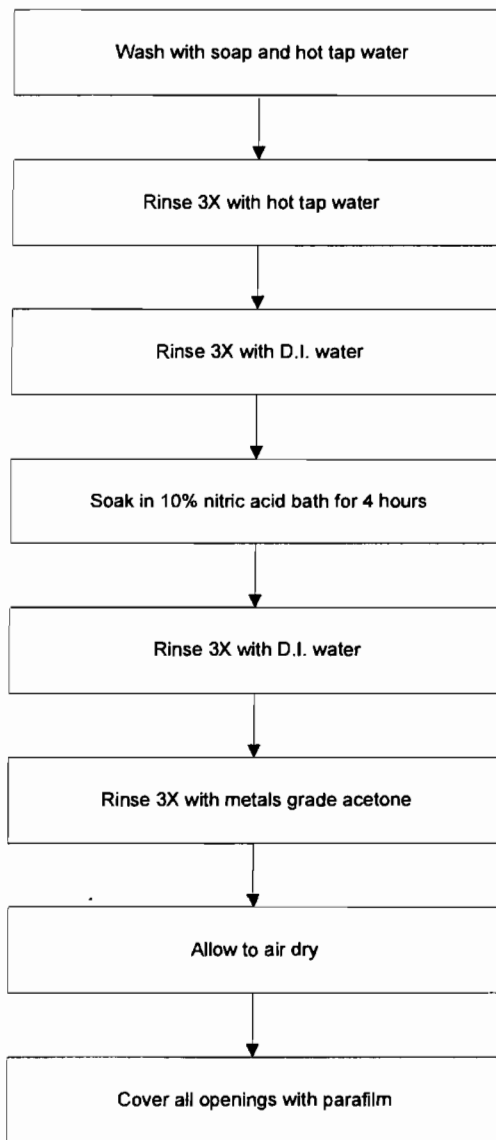
## EPA Method 29 Sampling Train Configuration



### Impinger Contents

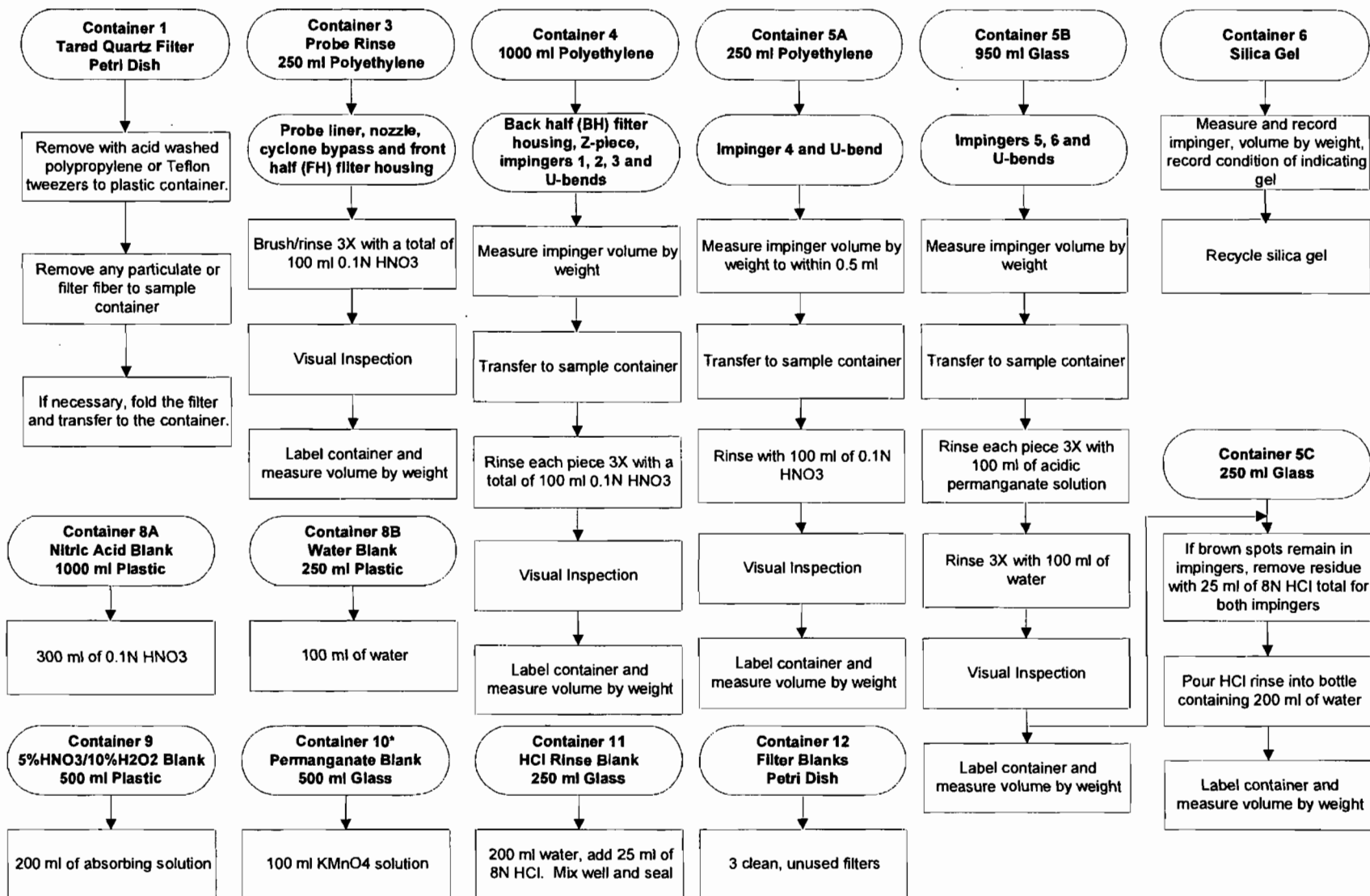
Impinger 1	Empty
Impinger 2	100 ml 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>
Impinger 3	100 ml 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>
Impinger 4	Empty
Impinger 5	100 ml 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>
Impinger 6	100 ml 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>
Impinger 7	Silica Gel

## EPA Method 29 Glassware Preparation Procedures

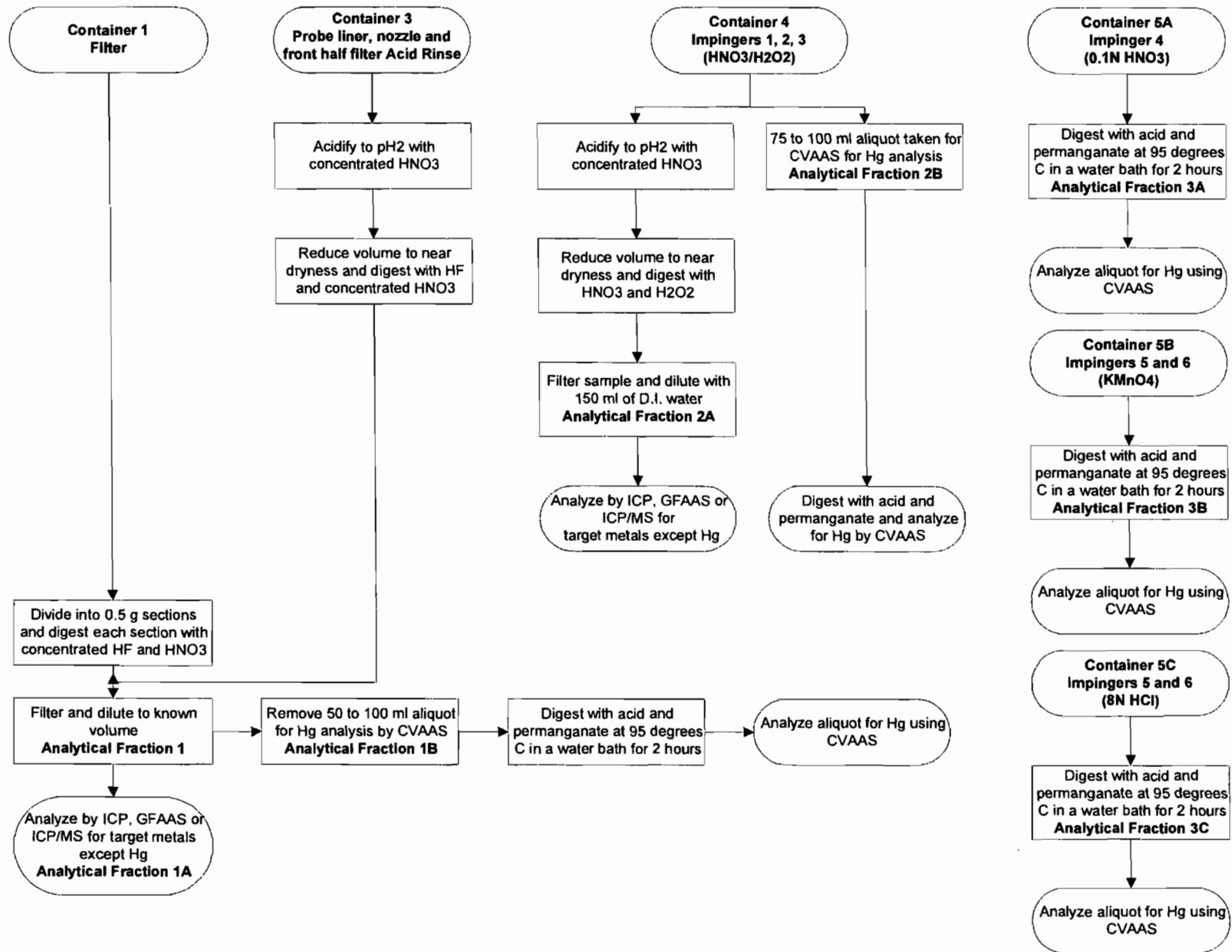


## EPA Method 29 Sample Recovery Flowchart (includes Mercury)

- Tare all sample containers before sample collection
- Mark all liquid levels and final weights on the outside of each sample container
- Seal all sample containers with Teflon tape
- If recycling, bake silica gel for two hours at 350 degrees F (175 degrees C)
- Collect one complete blank set per field test



**EPA Method 29  
Analytical Flowchart  
(includes Mercury)**



WHEELABRATOR NORTH BROWARD, INC.  
POMPANO BEACH, FL

Client Reference No: 14800198  
CleanAir Project No: 10455-6

**SAMPLE CALCULATIONS**

**B**

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Wheelabrator North Broward, Inc.  
 Clean Air Project No: 10455  
 Unit 1 FF Outlet

**USEPA Method 29 (Trace Metals)  
 Sampling, Velocity and Moisture Sample Calculations**

Sample data taken from Run 1

*Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.*

071808 140121  
 S

1. Volume of water collected (wscf)

$$V_{wstd} = (0.04707)(V_{lc})$$

Where:

$V_{lc}$	= total volume of liquid collected in impingers and silica gel (ml)	=	459.3	ml
0.04707	= ideal gas conversion factor (ft <sup>3</sup> water vapor/ml or gm)	=	0.04707	ft <sup>3</sup> /ml
$V_{wstd}$	= volume of water vapor collected at standard conditions (ft <sup>3</sup> )	=	21.62	ft <sup>3</sup>

2. Volume of gas metered, standard conditions (dscf)

$$V_{mstd} = \frac{(17.64)(V_m) \left( P_{bar} + \frac{\Delta H}{13.6} \right) (Y_d)}{(460 + T_m)}$$

Where:

$P_{bar}$	= barometric pressure (in. Hg)	=	30.07	in. Hg
$T_m$	= average dry gas meter temperature (°F)	=	94.72	°F
$V_m$	= volume of gas sample through the dry gas meter at meter conditions (dcf)	=	74.51	dcf
$Y_d$	= gas meter correction factor (dimensionless)	=	0.9842	
$\Delta H$	= average pressure drop across meter box orifice (in. H <sub>2</sub> O)	=	1.12	in. H <sub>2</sub> O
17.64	= standard temperature to pressure ratio (°R/in. Hg)	=	17.64	°R/in. Hg
13.6	= conversion factor (in. H <sub>2</sub> O/in. Hg)	=	13.6	in. H <sub>2</sub> O/in. Hg
460	= °F to °R conversion constant	=	460	
$V_{mstd}$	= volume of gas sampled through the dry gas meter at standard conditions (dscf)	=	70.314	dscf

3. Sample gas pressure (in. Hg)

$$P_s = P_{bar} + \left( \frac{P_g}{13.6} \right)$$

Where:

$P_{bar}$	= barometric pressure (in. Hg)	=	30.07	in. Hg
$P_g$	= sample gas static pressure (in. H <sub>2</sub> O)	=	-10.80	in. H <sub>2</sub> O
13.6	= conversion factor (in. H <sub>2</sub> O/in. Hg)	=	13.6	in. H <sub>2</sub> O/in. Hg
$P_s$	= absolute sample gas pressure (in. Hg)	=	29.28	in. Hg

Wheelabrator North Broward, Inc.  
 Clean Air Project No: 10455  
 Unit 1 FF Outlet

4. Actual water vapor pressure at sample gas temperature less than 212°F (in. Hg)

$$P_v = \frac{e^{\left( \frac{18.3036 - \frac{3816.44}{\frac{5}{9}(T_s - 32) + 273.15 - 46.13}}{25.4} \right)}}{25.4}$$

Where:

$T_s$	= average sample gas temperature (°F)	=	310.12	°F
18.3036	= Antoine coefficient	=	18.3036	°K
3816.44	= Antoine coefficient	=	3816.44	°K
273.15	= temperature conversion factor	=	273.15	°K
46.13	= Antoine coefficient	=	46.13	°K
25.4	= conversion factor	=	25.4	mm Hg/in. Hg
5/9	= Fahrenheit to Celsius conversion factor	=	5/9	°C/°F
32	= temperature conversion (°F)	=	32	°F
$P_v$	= vapor pressure, actual (in. Hg)	=	29.28	in. Hg

5. Water vapor pressure at gas temperature greater than 212°F (in. Hg)

$$P_v = P_s$$

Where:

$P_s$	= absolute sample gas pressure (in. Hg)	=	29.28	in. Hg
$P_v$	= water vapor pressure, actual (in. Hg)	=	29.28	in. Hg

6. Moisture measured in sample (% by volume)

$$B_{wo} = \frac{V_{wstd}}{(V_{mstd} + V_{wstd})}$$

Where:

$V_{mstd}$	= volume of gas sampled through the dry gas meter at standard conditions (dscf)	=	70.314	dscf
$V_{wstd}$	= volume of water collected at standard conditions (scf)	=	21.62	scf
$B_{wo}$	= proportion of water measured in the gas stream by volume	=	0.2352	
		=	23.52	%

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7. Saturated moisture content (% by volume)

$$B_{ws} = \frac{P_v}{P_s}$$

Where:

$P_s$	= absolute sample gas pressure (in. Hg)	=	29.28	in. Hg
$P_v$	= water vapor pressure, actual (in. Hg)	=	29.28	in. Hg
$B_{ws}$	= proportion of water vapor in the gas stream by volume at saturated conditions	=	1.0000	%
			100.00	%

8. Actual water vapor in gas (% by volume)

$$B_w = \text{MINIMUM} [B_{wo}, B_{ws}]$$

Where:

$B_{ws}$	= proportion of water vapor in the gas stream by volume at saturated conditions	=	1.0000	
$B_{wo}$	= proportion of water measured in the gas stream by volume	=	0.2352	
$B_w$	= actual water vapor in gas	=	0.2352	%
		=	23.52	%

9. Nitrogen (plus carbon monoxide) in gas stream (% by volume, dry)

$$N_2 + CO = 100 - CO_2 - O_2$$

Where:

$CO_2$	= proportion of carbon dioxide in the gas stream by volume (%)	=	10.6	%
$O_2$	= proportion of oxygen in the gas stream by volume (%)	=	8.8	%
100	= conversion factor (%)	=	100	%
$N_2+CO$	= proportion of nitrogen and CO in the gas stream by volume (%)	=	80.60	%

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10. Molecular weight of dry gas stream (lb/lb-mole)

$$M_d = (M_{CO_2}) \left( \frac{CO_2}{100} \right) + (M_{O_2}) \left( \frac{O_2}{100} \right) + (M_{N_2+CO}) \left( \frac{N_2+CO}{100} \right)$$

Where:

$M_{CO_2}$	= molecular weight of carbon dioxide (lb/lb-mole)	=	44.00	lb/lb-mole
$M_{O_2}$	= molecular weight of oxygen (lb/lb-mole)	=	32.00	lb/lb-mole
$M_{N_2+CO}$	= molecular weight of nitrogen and carbon monoxide (lb/lb-mole)	=	28.00	lb/lb-mole
$CO_2$	= proportion of carbon dioxide in the gas stream by volume (%)	=	10.6	%
$O_2$	= proportion of oxygen in the gas stream by volume (%)	=	8.8	%
$N_2+CO$	= proportion of nitrogen and CO in the gas stream by volume (%)	=	80.6	%
100	= conversion factor (%)	=	100	%
$M_d$	= dry molecular weight of sample gas (lb/lb-mole)	=	30.05	lb/lb-mole

11. Molecular weight of sample gas (lb/lb-mole)

$$M_s = (M_d)(1 - B_w) + (M_{H_2O})(B_w)$$

Where:

$B_w$	= proportion of water vapor in the gas stream by volume	=	0.2352	
$M_d$	= dry molecular weight of sample gas (lb/lb-mole)	=	30.05	lb/lb-mole
$M_{H_2O}$	= molecular weight of water (lb/lb-mole)	=	18.00	lb/lb-mole
$M_s$	= molecular weight of sample gas, wet basis (lb/lb-mole)	=	27.21	lb/lb-mole

12. Velocity of sample gas (ft/sec)

$$V_s = (K_p)(C_p) \left( \sqrt{\Delta P} \right) \left( \sqrt{\frac{(T_s + 460)}{(M_s)(P_s)}} \right)$$

Where:

$K_p$	= velocity pressure constant	=	85.49	
$C_p$	= pitot tube coefficient	=	0.84	
$M_s$	= wet molecular weight of sample gas, wet basis (lb/lb-mole)	=	27.21	lb/lb-mole
$P_s$	= absolute sample gas pressure (in. Hg)	=	29.28	in. Hg
$T_s$	= average sample gas temperature (°F)	=	310.12	°F
$\sqrt{\Delta P}$	= average square roots of velocity heads of sample gas (in. H <sub>2</sub> O)	=	0.682	in. H <sub>2</sub> O
460	= °F to °R conversion constant	=	460	
$V_s$	= sample gas velocity (ft/sec)	=	48.16	ft/sec

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13. Volumetric flow rate of sample gas at actual gas conditions (acfm)

$$Q_a = (60)(A_s)(V_s)$$

Where:

$A_s$	= cross sectional area of sampling location (ft <sup>2</sup> )	=	64.00	ft <sup>2</sup>
$V_s$	= sample gas velocity (ft/sec)	=	48.16	ft/sec
60	= conversion factor (sec/min)	=	60	sec/min

$Q_a$	= volumetric flow rate at actual conditions (acfm)	=	184,949	acfm
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14. Total flow of sample gas (scfm)

$$Q_s = (Q_a) \left( \frac{P_s}{29.92} \right) \left( \frac{68 + 460}{T_s + 460} \right)$$

Where:

$Q_a$	= volumetric flow rate at actual conditions (acfm)	=	184,949	acfm
$P_s$	= absolute sample gas pressure (in. Hg)	=	29.28	in. Hg
29.92	= standard pressure (in. Hg)	=	29.92	in. Hg
$T_s$	= average sample gas temperature (°F)	=	310.1	°F
68	= standard temperature (°F)	=	68	°F
460	= °F to °R conversion constant	=	460	

$Q_s$	= volumetric flow rate at standard conditions, wet basis (scfm)	=	124,072	scfm
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15. Dry flow of sample gas (dscfm)

$$Q_{std} = (Q_s)(1 - B_w)$$

Where:

$B_w$	= proportion of water vapor in the gas stream by volume	=	0.2352	
$Q_s$	= volumetric flow rate at standard conditions, wet basis (scfm)	=	124,072	scfm

$Q_{std}$	= volumetric flow rate at standard conditions, dry basis (dscfm)	=	94,895	dscfm
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16. Dry flow of sample gas corrected to 7%O<sub>2</sub> (dscfm)

$$Q_{std7} = (Q_{std}) \left( \frac{20.9 - O_2}{20.9 - 7} \right)$$

Where:

$Q_{std}$	= volumetric flow rate at standard conditions, dry basis (dscfm)	=	94,895	dscfm
$O_2$	= proportion of oxygen in the gas stream by volume (%)	=	8.8	%
20.9	= oxygen content of ambient air (%)	=	20.9	%
7	= oxygen content of corrected gas (%)	=	7.0	%

$Q_{std7}$	= volumetric flow rate at STP and 7%O <sub>2</sub> , dry basis (dscfm)	=	82,606	dscfm
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17. Hourly time basis conversion of volumetric flow rate ( $Q_{std}$  example)

$$Q_{std-hr} = (Q_{std-min})(60)$$

Where

$Q_{std-min}$	= volumetric flow rate, english units (ft <sup>3</sup> /min)	=	94,895	dscfm
60	= conversion factor (min/hr)	=	60	min/hr

$Q_{std-hr}$	= volumetric flow rate, hourly basis (dscf/hr)	=	5,693,704	dscf/hr
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18. Metric Conversion of Gas Volumes ( $Q_{std}$  example)

$$Q_{std-metric} = (Q_{std-english}) \left( \frac{60}{35.31} \right)$$

Where:

$Q_{std-english}$	= volumetric flow rate, english units (ft <sup>3</sup> /min)	=	94,895	dscfm
35.31	= conversion factor (ft <sup>3</sup> /m <sup>3</sup> )	=	35.31	ft <sup>3</sup> /m <sup>3</sup>
60	= conversion factor (min/hr)	=	60	min/hr

$Q_{std-metric}$	= volumetric flow rate, metric units (m <sup>3</sup> /hr)	=	161,249	dry std m <sup>3</sup> /hr
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19. Standard to Normal Conversion of Gas Volumes ( $Q_{std}$  example)

$$Q_{Normal} = (Q_{std-metric}) \left( \frac{32 + 460}{68 + 460} \right)$$

Where:

$Q_{std-metric}$	= volumetric flow rate, metric units (dry std m <sup>3</sup> /hr)	=	161,249	dry std m <sup>3</sup> /hr
32	= normal temperature (°F)	=	32	°F
68	= standard temperature (°F)	=	68	°F
460	= standard temperature in Rankine (68°F)	=	460	

$Q_{Normal}$	= volumetric flow rate, metric units (dry Nm <sup>3</sup> /hr)	=	150,255	dry Nm <sup>3</sup> /hr
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20. Percent isokinetic (%)

$$I = \frac{(0.09450)(\bar{T}_s + 460)(V_{mstd})}{(P_s)(V_s)\left(\frac{D_n}{1.44}\right)^2 \left(\frac{\pi}{4}\right) \Theta (1 - B_w)}$$

Where:

$D_n$	= diameter of nozzle (in)	=	0.264	in.
$B_w$	= proportion of water vapor in the gas stream by volume	=	0.2352	
$P_s$	= absolute sample gas pressure (in. Hg)	=	29.28	in. Hg
$T_s$	= average sample gas temperature (°F)	=	310.1	°F
$V_{mstd}$	= volume of gas sample through the dry gas meter at standard conditions (dscf)	=	70.314	dscf
$V_s$	= sample gas velocity (ft/sec)	=	48.16	ft/sec
$\theta$	= total sampling time (min)	=	125	min
0.0945	= conversion constant	=	0.0945	
460	= °F to °R conversion constant	=	460	
$I$	= percent of isokinetic sampling (%)	=	99.86	%

21. Alternative Method 5 Post-Test Meter Calibration Factor

$$Y_{qa} = \frac{\Theta}{V_m} \sqrt{\frac{(0.0319)(T_m + 460)(28.96)}{(\Delta H_{\Theta})(P_{bar} + \frac{\Delta H}{13.6})(M_d)}} (\sqrt{\Delta H})_{avg}$$

Where:

$\theta$	= total sampling time (min)	=	125	min
$V_m$	= volume of gas sample through the dry gas meter at meter conditions (dcf)	=	74.51	dcf
$T_m$	= average dry gas meter temperature (°F)	=	94.72	°F
$\Delta H_{\Theta}$	= dry gas meter orifice coefficient	=	1.8163	
$P_{bar}$	= barometric pressure (in. Hg)	=	30.07	in. Hg
$\Delta H$	= average pressure drop across meter box orifice (in. H <sub>2</sub> O)	=	1.117	in. H <sub>2</sub> O
$M_d$	= dry molecular weight of sample gas (lb/lb-mole)	=	30.05	lb/lb-mole
$\sqrt{\Delta H}_{avg}$	= average of square root of pressure drop across meter orifice	=	1.054	$\sqrt{\text{in. H}_2\text{O}}$
0.0319	= conversion constant	=	0.0319	
28.96	= molecular weight of ambient air (lb/lb-mole)	=	28.96	lb/lb-mole
13.6	= conversion factor (in. H <sub>2</sub> O/in. Hg)	=	13.6	in.H <sub>2</sub> O/in. Hg
460	= °F to °R conversion constant	=	460	
$Y_{qa}$	= alternative Method 5 post-test meter calibration factor	=	0.9863	

## LOGIC FOR TREATING DETECTION LIMITS

(mercury only)

### 1. Logic for Determining Total Blank ( $m_{\text{Total-B}}$ ) from 5 Fractions

	<b>CASE 1</b>	<b>CASE 2</b>	<b>CASE 3</b>
	All 5 fractions are D.	1 to 4 fractions are ND	All 5 fractions are ND
<b>Rule</b>			
$ND = 0$	$m_{\text{Total-B}} = \text{Sum D, 1-5}$	$m_{\text{Total-B}} = \text{Sum D}$	$m_{\text{Total-B}} = < \text{Sum ND}$
$ND = 1x$	$m_{\text{Total-B}} = \text{Sum D, 1-5}$	$m_{\text{Total-B}} = \text{Sum D}$	$m_{\text{Total-B}} = < \text{Sum ND}$
$ND = 0.5x$	$m_{\text{Total-B}} = \text{Sum D, 1-5}$	$m_{\text{Total-B}} = \text{Sum D}$	$m_{\text{Total-B}} = < 0.5 \text{ Sum ND}$

### 2. Logic for Determining Total Sample ( $m_{\text{Total-S}}$ ) from 5 Fractions

	<b>CASE 1</b>	<b>CASE 2</b>	<b>CASE 3</b>
	All 5 fractions are D.	1 to 4 fractions are ND	All 5 fractions are ND
<b>Rule</b>			
$ND = 0$	$m_{\text{Total-S}} = \text{Sum D, 1-5}$	$m_{\text{Total-S}} = \text{Sum D}$	$m_{\text{Total-S}} = < \text{Sum ND}$
$ND = 1x$	$m_{\text{Total-S}} = \text{Sum D, 1-5}$	$m_{\text{Total-S}} = < [\text{Sum D} + \text{Sum ND}]$	$m_{\text{Total-S}} = < \text{Sum ND}$
$ND = 0.5x$	$m_{\text{Total-S}} = \text{Sum D, 1-5}$	$m_{\text{Total-S}} = < [\text{Sum D} + 0.5 \text{ Sum ND}]$	$m_{\text{Total-S}} = < 0.5 \text{ Sum ND}$

### 3. Logic for Determining Maximum Allowable Blank Correction ( $m_{\text{T-B-allow}}$ )

	<b>CASE 1</b>	<b>CASE 2</b>	<b>CASE 3</b>	<b>CASE 4</b>
	All 5 fractions are D.	1 to 4 sample fractions are ND	All 5 fractions are ND	Any type of fractions
	$m_{\text{Total-B}} = D$	$m_{\text{Total-B}} = D$	$m_{\text{Total-B}} = D$	$m_{\text{Total-B}} = ND$
<b>Rule</b>				
$ND = 0$	$m_{\text{T-B-allow}} = \text{M29 Rule}$	$m_{\text{T-B-allow}} = \text{M29 Rule}^*$	$m_{\text{T-B-allow}} = 0$	$m_{\text{T-B-allow}} = 0$
$ND = 1x$	$m_{\text{T-B-allow}} = \text{M29 Rule}$	$m_{\text{T-B-allow}} = \text{M29 Rule}^*$	$m_{\text{T-B-allow}} = 0$	$m_{\text{T-B-allow}} = 0$
$ND = 0.5x$	$m_{\text{T-B-allow}} = \text{M29 Rule}$	$m_{\text{T-B-allow}} = \text{M29 Rule}^*$	$m_{\text{T-B-allow}} = 0$	$m_{\text{T-B-allow}} = 0$

\* M29 rule using only detected sample quantities for logical comparisons.

### 4. Logic for Determining Blank-Corrected Sample Amount ( $m_n$ )

	<b>CASE 1</b>	<b>CASE 2</b>	<b>CASE 3</b>	<b>CASE 4</b>
	All 5 fractions are D.	1 to 4 sample fractions are ND	All 5 fractions are ND	Any type of fractions
	$m_{\text{Total-S}} - m_{\text{T-B-allow}} \geq \text{MIN}(\text{MDL})$	$m_{\text{Total-S}} - m_{\text{T-B-allow}} \geq \text{MIN}(\text{MDL})$	$m_{\text{Total-S}}$ and $m_{\text{T-B-allow}}$ anything	$m_{\text{Total-S}} - m_{\text{T-B-allow}} < \text{MIN}(\text{MDL})$
<b>Rule</b>				
$ND = 0$	$m_n = m_{\text{Total-S}} - m_{\text{T-B-allow}}$	$m_n = m_{\text{Total-S}} - m_{\text{T-B-allow}}$	$m_n = < m_{\text{Total-S}}$	$m_n = < \text{MIN}[\text{MDL}]$
$ND = 1x$	$m_n = m_{\text{Total-S}} - m_{\text{T-B-allow}}$	$m_n = < [m_{\text{Total-S}} - m_{\text{T-B-allow}}]$	$m_n = < m_{\text{Total-S}}$	$m_n = < \text{MIN}[\text{MDL}]$
$ND = 0.5x$	$m_n = m_{\text{Total-S}} - m_{\text{T-B-allow}}$	$m_n = < [m_{\text{Total-S}} - m_{\text{T-B-allow}}]$	$m_n = < m_{\text{Total-S}}$	$m_n = < \text{MIN}[\text{MDL}]$

#### Definitions and Notes

The term "Rule" refers to the rule being implemented for handling non-detectable quantities in summations.

MDL = minimum detection limit.

D = Detectable quantity reported as D.

ND = Non-Detectable quantity reported at a value of ND.

MIN[MDL] = lowest quantity of all detection limits for 5 fractions.



**USEPA Method 29  
 Mercury Analyte Calculations**

**Sample data taken from Run 1**

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

Note: Please see the preceding page concerning treatment of minimum detection limits and mathematical operations on values that are below minimum detection limits.

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**1. Total blank amount ( $\mu\text{g}$ )**

$$m_{\text{total-B}} = \sum_{i=1}^n m_{i-B}$$

Where:

$m_{1b-B}$	= mercury amount in blank for Fraction 1b	=	<0.1000	$\mu\text{g}$
$m_{2b-B}$	= mercury amount in blank for Fraction 2b	=	<0.2000	$\mu\text{g}$
$m_{3a-B}$	= mercury amount in blank for Fraction 3a	=	<0.2000	$\mu\text{g}$
$m_{3b-B}$	= mercury amount in blank for Fraction 3b	=	<0.5000	$\mu\text{g}$
$m_{3c-B}$	= mercury amount in blank for Fraction 3c	=	<0.4000	$\mu\text{g}$
$m_{\text{total-B}}$	= total amount of mercury in blank	=	<1.4000	$\mu\text{g}$

**2. Total sample amount ( $\mu\text{g}$ )**

$$m_{\text{total-S}} = \sum_{i=1}^n m_{i-S}$$

Where:

$m_{1b-S}$	= mercury amount in sample for Fraction 1b	=	<0.1000	$\mu\text{g}$
$m_{2b-S}$	= mercury amount in sample for Fraction 2b	=	18.9204	$\mu\text{g}$
$m_{3a-S}$	= mercury amount in sample for Fraction 3a	=	<0.2000	$\mu\text{g}$
$m_{3b-S}$	= mercury amount in sample for Fraction 3b	=	<0.5000	$\mu\text{g}$
$m_{3c-S}$	= mercury amount in sample for Fraction 3c	=	<0.4000	$\mu\text{g}$
$m_{\text{total-S}}$	= total amount of mercury in sample	=	18.9204	$\mu\text{g}$

**3. Allowable blank correction ( $\mu\text{g}$ )**

$$m_{T-B-\text{allow}} = m_{\text{total-B}} \text{ if } m_{\text{total-B}} \leq 0.6$$

$$m_{T-B-\text{allow}} = \text{MAX} [0.6, \text{MIN} (m_{\text{total-B}}, 0.05 \times m_{\text{total-S}})] \text{ if } m_{\text{total-B}} > 0.6$$

Where:

$m_{\text{total-B}}$	= total amount of mercury in blank	=	<1.4000	$\mu\text{g}$
$m_{\text{total-S}}$	= total amount of mercury in sample	=	18.9204	$\mu\text{g}$
$0.05 \times m_{\text{total-S}}$	= 5% of $m_{\text{total-S}}$	=	0.9460	$\mu\text{g}$
MAX	= arithmetic operator that returns the maximum of two values			
MIN	= arithmetic operator that returns the minimum of two values			

$m_{T-B-\text{allow}}$	= total allowable blank correction	=	0.0000	$\mu\text{g}$
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NOTE: In this case, the second criteria applies.

4. Sample corrected for allowable blank - Total (µg)

$$m_n = m_{total-S} - m_{T-B-allow}$$

Where:

$m_{total-S}$	= total amount of mercury in sample	=	18.9204	µg
$m_{T-B-allow}$	= total allowable blank correction	=	0.0000	µg
$m_n$	= total mercury in sample corrected for allowable blank	=	18.9204	µg

5. Sample corrected for allowable blank - Prorated for each fraction (µg)

$$m_{n-i} = \left( \frac{m_{i-S}}{m_{total-S}} \right) (m_n)$$

Where:

$m_n$	= total mercury in sample corrected for allowable blank	=	18.9204	µg
$m_{1b-S}$	= mercury amount in sample for Fraction 1b	=	<0.1000	µg
$m_{2b-S}$	= mercury amount in sample for Fraction 2b	=	18.9204	µg
$m_{3a-S}$	= mercury amount in sample for Fraction 3a	=	<0.2000	µg
$m_{3b-S}$	= mercury amount in sample for Fraction 3b	=	<0.5000	µg
$m_{3c-S}$	= mercury amount in sample for Fraction 3c	=	<0.4000	µg
$m_{total-S}$	= total amount of mercury in sample	=	18.9204	µg
$m_{n-1b}$	= mercury corrected for blank - prorated for Fraction 1b	=	<0.1000	µg
$m_{n-2b}$	= mercury corrected for blank - prorated for Fraction 2b	=	18.9204	µg
$m_{n-3a}$	= mercury corrected for blank - prorated for Fraction 3a	=	<0.2000	µg
$m_{n-3b}$	= mercury corrected for blank - prorated for Fraction 3b	=	<0.5000	µg
$m_{n-3c}$	= mercury corrected for blank - prorated for Fraction 3c	=	<0.4000	µg

**USEPA Method 29  
 Mercury Sample Calculations**

**Sample data taken from Run 1**

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1. Mercury concentration (lb/dscf)

$$C_{sd} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{2.205 \times 10^{-3}}{10^6} \right)$$

Where:

$m_n$	= mercury collected in sample (total $\mu\text{g}$ )	= 18.9204 $\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	= 70.3138 dscf
$2.205 \times 10^{-3}$	= conversion factor (lb/g)	= 2.205E-03 lb/g
$10^6$	= conversion factor ( $\mu\text{g/g}$ )	= 1.0E+06 $\mu\text{g/g}$
$C_{sd}$	= mercury concentration (lb/dscf)	= 5.9333E-10 lb/dscf

2. Mercury concentration ( $\mu\text{g/dscm}$ )

$$C_{sd} = \left( \frac{m_n}{V_{mstd}} \right) (35.31)$$

Where:

$m_n$	= mercury collected in sample (total $\mu\text{g}$ )	= 18.9204 $\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	= 70.3138 dscf
35.31	= conversion factor (dscf/dscm)	= 35.31 dscf/dscm
$C_{sd}$	= mercury concentration ( $\mu\text{g/dscm}$ )	= 9.5014E+00 $\mu\text{g/dscm}$

3. Mercury concentration (mg/dscm)

$$C_{sd} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{35.31}{1000} \right)$$

Where:

$m_n$	= mercury collected in sample (total $\mu\text{g}$ )	= 18.9204 $\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	= 70.3138 dscf
35.31	= conversion factor (dscf/dscm)	= 35.31 dscf/dscm
1000	= conversion factor ( $\mu\text{g/mg}$ )	= 1000 $\mu\text{g/mg}$
$C_{sd}$	= mercury concentration (mg/dscm)	= 9.5014E-03 mg/dscm

4. Mercury concentration ( $\mu\text{g}/\text{Nm}^3$  dry)

$$C_{sd} = \left( \frac{m_n}{V_{mstd}} \right) (35.31) \left( \frac{68 + 460}{32 + 460} \right)$$

Where:

$m_n$	= mercury collected in sample (total $\mu\text{g}$ )	= 18.9204	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	= 70.3138	dscf
35.31	= conversion factor (dscf/dscm)	= 35.31	dscf/dscm
68	= standard temperature ( $^{\circ}\text{F}$ )	= 68	$^{\circ}\text{F}$
32	= normal temperature ( $^{\circ}\text{F}$ )	= 32	$^{\circ}\text{F}$
460	= $^{\circ}\text{F}$ to $^{\circ}\text{R}$ conversion constant	= 460	

$C_{sd}$	= mercury concentration ( $\mu\text{g}/\text{Nm}^3$ dry)	= 1.0197E+01	$\mu\text{g}/\text{Nm}^3$ dry
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5. Mercury concentration corrected to x% oxygen (lb/dscf example)

$$C_{sdx} = C_{sd} \left( \frac{20.9 - x}{20.9 - O_2} \right)$$

Where:

$C_{sd}$	= mercury concentration (lb/dscf)	= 5.9333E-10	lb/dscf
x	= oxygen content of corrected gas (%)	= 7.0	%
$O_2$	= proportion of oxygen in the gas stream by volume (%)	= 8.8	%
20.9	= oxygen content of ambient air (%)	= 20.9	%
$C_{sdx}$	= mercury concentration corrected to x% oxygen (lb/dscf)	= 6.8160E-10	lb/dscf @ x% $O_2$

6. Mercury concentration corrected to y% carbon dioxide (lb/dscf example)

$$C_{sdy} = C_{sd} \left( \frac{y}{CO_2} \right)$$

Where:

$C_{sd}$	= mercury concentration (lb/dscf)	= 5.9333E-10	lb/dscf
y	= carbon dioxide content of corrected gas (%)	= 12.0	%
$CO_2$	= proportion of carbon dioxide in the gas stream by volume (%)	= 10.6	%
$C_{sdy}$	= mercury conc. corrected to y% carbon dioxide (lb/dscf)	= 6.7170E-10	lb/dscf @ y% $CO_2$

7. Mercury concentration at actual gas conditions (lb/acf example)

$$C_a = C_{sd} \left( \frac{Q_{std}}{Q_a} \right)$$

Where:

$C_{sd}$	= mercury concentration (lb/dscf)	= 5.9333E-10	lb/dscf
$Q_{std}$	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 94,895	dscfm
$Q_a$	= volumetric flow rate at actual conditions (acfm)	= 184,949	acfm
$C_a$	= mercury concentration at actual gas conditions (lb/acf)	= 3.0443E-10	lb/acf

8. Mercury emission rate (lb/hr)

$$E_{lb/hr} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{2.205 \times 10^{-3}}{10^6} \right) (Q_{std}) (60)$$

Where:

$m_n$	= mercury collected in sample (total $\mu\text{g}$ )	= 18.9204	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	= 70.3138	dscf
$2.205 \times 10^{-3}$	= conversion factor (lb/g)	= 2.205E-03	lb/g
$10^6$	= conversion factor ( $\mu\text{g/g}$ )	= 1.0E+06	$\mu\text{g/g}$
$Q_{std}$	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 94,895	dscfm
60	= conversion factor (min/hr)	= 60	min/hr
$E_{lb/hr}$	= mercury emission rate (lb/hr)	= 3.3783E-03	lb/hr

9. Mercury emission rate (g/s)

$$E_{g/s} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{Q_{std}}{(10^6)(60)} \right)$$

Where:

$m_n$	= mercury collected in sample (total $\mu\text{g}$ )	= 18.9204	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	= 70.3138	dscf
$Q_{std}$	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 94,895	dscfm
$10^6$	= conversion factor ( $\mu\text{g/g}$ )	= 1.0E+06	$\mu\text{g/g}$
60	= conversion factor (sec/min)	= 60	sec/min
$E_{g/s}$	= mercury emission rate (g/s)	= 4.2558E-04	g/s

10. Mercury emission rate (Ton/yr)

$$E_{T/yr} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{2.205 \times 10^{-3}}{10^6} \right) (Q_{std}) (60) \left( \frac{Cap}{2000} \right)$$

Where:

$m_n$	= mercury collected in sample (total $\mu\text{g}$ )	= 18.9204	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	= 70.3138	dscf
$2.205 \times 10^{-3}$	= conversion factor (lb/g)	= 2.205E-03	lb/g
$10^6$	= conversion factor ( $\mu\text{g/g}$ )	= 1.0E+06	$\mu\text{g/g}$
$Q_{std}$	= volumetric flow rate at standard conditions, dry basis (dscfm)	= 94,895	dscfm
60	= conversion factor (min/hr)	= 60	min/hr
Cap	= capacity factor for process (hours operated/year)	= 8,760	hours/yr
2000	= conversion factor (lb/Ton)	= 2000	lb/Ton
$E_{T/yr}$	= mercury emission rate (Ton/yr)	= 1.4797E-02	Ton/yr

11. Mercury emission rate - Fd-based (lb/MMBtu)

$$E_{Fd} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{2.205 \times 10^{-3}}{10^6} \right) (F_d) \left( \frac{20.9}{20.9 - O_2} \right)$$

Where:

$m_n$	= mercury collected in sample (total $\mu\text{g}$ )	= 18.9204	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	= 70.3138	dscf
$2.205 \times 10^{-3}$	= conversion factor (lb/g)	= 2.205E-03	lb/g
$10^6$	= conversion factor ( $\mu\text{g}/\text{g}$ )	= 1.0E+06	$\mu\text{g}/\text{g}$
$F_d$	= ratio of gas volume to heat content of fuel (dscf/MMBtu)	= 9,570	dscf/MMBtu
$O_2$	= proportion of oxygen in the gas stream by volume (%)	= 8.8	%
20.9	= oxygen content of ambient air (%)	= 20.9	%
$E_{Fd}$	= mercury emission rate - Fd-based (lb/MMBtu)	= 9.8078E-06	lb/MMBtu

12. Mercury emission rate - Fc-based (lb/MMBtu)

$$E_{Fc} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{2.205 \times 10^{-3}}{10^6} \right) (F_c) \left( \frac{100}{CO_2} \right)$$

Where:

$m_n$	= mercury collected in sample (total $\mu\text{g}$ )	= 18.9204	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	= 70.3138	dscf
$2.205 \times 10^{-3}$	= conversion factor (lb/g)	= 2.205E-03	lb/g
$10^6$	= conversion factor ( $\mu\text{g}/\text{g}$ )	= 1.0E+06	$\mu\text{g}/\text{g}$
$F_c$	= ratio of gas volume to heat content of fuel (dscf/MMBtu)	= 1,820	dscf/MMBtu
$CO_2$	= proportion of oxygen in the gas stream by volume (%)	= 10.6	%
100	= conversion factor	= 100	
$E_{Fc}$	= mercury emission rate - Fc-based (lb/MMBtu)	= 1.0187E-05	lb/MMBtu

WHEELABRATOR NORTH BROWARD, INC.  
POMPANO BEACH, FL

Client Reference No: 14800198  
CleanAir Project No: 10455-6

**PARAMETERS**

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Wheelabrator North Broward, Inc.  
 Clean Air Project No: 10455  
 Unit 1 FF Outlet

**USEPA Method 29 (Trace Metals)  
 Sampling, Velocity and Moisture Parameters**

Run No.		1	2	3	Average
Date (2008)		Jun 27	Jun 27	Jun 27	
Start Time (approx.)		09:01	11:36	14:10	
Stop Time (approx.)		11:17	13:50	16:30	
<b>Sampling Conditions</b>					
Y <sub>d</sub>	Dry gas meter correction factor	0.9842	0.9842	0.9842	
C <sub>p</sub>	Pitot tube coefficient	0.84	0.84	0.84	
P <sub>g</sub>	Static pressure (in. H <sub>2</sub> O)	-10.8000	-10.8000	-10.8000	
A <sub>s</sub>	Sample location area (ft <sup>2</sup> )	64.0000	64.0000	64.0000	
P <sub>bar</sub>	Barometric pressure (in. Hg)	30.07	30.08	30.08	<b>30.0767</b>
D <sub>n</sub>	Nozzle diameter (in.)	0.2640	0.2640	0.2640	
O <sub>2</sub>	Oxygen (dry volume %)	8.8000	9.0000	9.0000	<b>8.9333</b>
CO <sub>2</sub>	Carbon dioxide (dry volume %)	10.6000	10.4000	10.2000	<b>10.4000</b>
N <sub>2</sub> +CO	Nitrogen plus carbon monoxide (dry volume %)	80.6000	80.6000	80.8000	<b>80.6667</b>
V <sub>lc</sub>	Total Liquid collected (ml)	459.30	456.50	451.20	
V <sub>m</sub>	Volume metered, meter conditions (ft <sup>3</sup> )	74.5100	77.4700	79.0600	
T <sub>m</sub>	Dry gas meter temperature (°F)	94.7200	100.7000	103.0600	
T <sub>s</sub>	Sample temperature (°F)	310.1200	311.0000	311.6000	<b>310.9067</b>
ΔH	Meter box orifice pressure drop (in. H <sub>2</sub> O)	1.1168	1.2004	1.2428	
θ	Total sampling time (min)	125.0	125.0	125.0	
<b>Flow Results</b>					
V <sub>wstd</sub>	Volume of water collected (ft <sup>3</sup> )	21.6193	21.4875	21.2380	<b>21.4482</b>
V <sub>mstd</sub>	Volume metered, standard (dscf)	70.3138	72.3661	73.5494	<b>72.0764</b>
P <sub>s</sub>	Sample gas pressure, absolute (in. Hg)	29.2759	29.2859	29.2859	<b>29.2825</b>
P <sub>v</sub>	Vapor pressure, actual (in. Hg)	29.2759	29.2859	29.2859	<b>29.2825</b>
B <sub>wo</sub>	Moisture measured in sample (% by volume)	23.5163	22.8947	22.4059	<b>22.9390</b>
B <sub>ws</sub>	Saturated moisture content (% by volume)	100.0000	100.0000	100.0000	<b>100.0000</b>
B <sub>w</sub>	Actual water vapor in gas (% by volume)	23.5163	22.8947	22.4059	<b>22.9390</b>
√ΔP	Velocity head (√in. H <sub>2</sub> O)	0.6822	0.7038	0.7189	<b>0.7016</b>
M <sub>d</sub>	MW of sample gas, dry (lb/lb-mole)	30.0480	30.0240	29.9920	<b>30.0213</b>
M <sub>w</sub>	MW of sample gas, wet (lb/lb-mole)	27.2148	27.2711	27.3051	<b>27.2637</b>
V <sub>s</sub>	Velocity of sample (ft/sec)	48.1637	49.6603	50.7124	<b>49.5121</b>
%I	Isokinetic sampling (%)	99.8589	98.9518	97.9393	<b>98.9167</b>
Q <sub>a</sub>	Volumetric flow rate, actual (acfm)	184,949	190,696	194,736	<b>190,127</b>
Q <sub>s</sub>	Volumetric flow rate, standard (scfm)	124,072	127,825	130,432	<b>127,443</b>
Q <sub>std</sub>	Volumetric flow rate, dry standard (dscfm)	94,895	98,560	101,207	<b>98,221</b>
Q <sub>std7</sub>	Volumetric flow rate, dry std@7%O <sub>2</sub> (dscfm)	82,606	84,379	86,645	<b>84,544</b>
Q <sub>a</sub>	Volumetric flow rate, actual (acf/hr)	11,096,911	11,441,739	11,684,140	<b>11,407,596</b>
Q <sub>s</sub>	Volumetric flow rate, standard (scf/hr)	7,444,337	7,669,522	7,825,916	<b>7,646,592</b>
Q <sub>std</sub>	Volumetric flow rate, dry standard (dscf/hr)	5,693,704	5,913,611	6,072,448	<b>5,893,254</b>
Q <sub>a</sub>	Volumetric flow rate, actual (m <sup>3</sup> /hr)	314,271	324,037	330,902	<b>323,070</b>
Q <sub>s</sub>	Volumetric flow rate, standard (m <sup>3</sup> /hr)	210,828	217,205	221,635	<b>216,556</b>
Q <sub>std</sub>	Volumetric flow rate, dry standard (dry m <sup>3</sup> /hr)	161,249	167,477	171,975	<b>166,900</b>
Q <sub>std7</sub>	Volumetric flow rate, dry std@7%O <sub>2</sub> (dry m <sup>3</sup> /hr)	140,368	143,380	147,231	<b>143,659</b>
Q <sub>s</sub>	Volumetric flow rate, normal (Nm <sup>3</sup> /hr)	196,453	202,396	206,523	<b>201,791</b>
Q <sub>std</sub>	Volumetric flow rate, dry normal (Nm <sup>3</sup> /hr)	150,255	156,058	160,250	<b>155,521</b>
Q <sub>std7</sub>	Volumetric flow rate, dry normal @7%O <sub>2</sub> (Nm <sup>3</sup> /hr)	130,797	133,604	137,192	<b>133,864</b>

**Comments:**

Average includes 3 runs.

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Wheelabrator North Broward, Inc.  
 Clean Air Project No: 10455  
 Unit 1 FF Outlet

**USEPA Method 29  
 Mercury (Hg) Emission Parameters**

Run No.	1	2	3	Average
Date (2008)	Jun 27	Jun 27	Jun 27	
Start Time (approx.)	09:01	11:36	14:10	
Stop Time (approx.)	11:17	13:50	16:30	
<b>Process Conditions</b>				
R <sub>p</sub> Steam Production Rate (Klbs/hour)	185	184	184	184
P <sub>1</sub> SDA Outlet Temperature (°F)	325	325	326	325
<b>Gas Conditions</b>				
O <sub>2</sub> Oxygen (dry volume %)	8.8000	9.0000	9.0000	8.9333
CO <sub>2</sub> Carbon dioxide (dry volume %)	10.6000	10.4000	10.2000	10.4000
T <sub>s</sub> Sample temperature (°F)	310.1200	311.0000	311.6000	310.9067
B <sub>w</sub> Actual water vapor in gas (% by volume)	23.5163	22.8947	22.4059	22.9390
<b>Gas Flow Rate</b>				
Q <sub>a</sub> Volumetric flow rate, actual (acfm)	184,949	190,696	194,736	190,127
Q <sub>a</sub> Volumetric flow rate, standard (scfm)	124,072	127,825	130,432	127,443
Q <sub>std</sub> Volumetric flow rate, dry standard (dscfm)	94,895	98,560	101,207	98,221
Q <sub>std7</sub> Volumetric flow rate, dry std@7%O <sub>2</sub> (dscfm)	82,606	84,379	86,645	84,544
Q <sub>a</sub> Volumetric flow rate, actual (acf/hr)	11,096,911	11,441,739	11,684,140	11,407,596
Q <sub>s</sub> Volumetric flow rate, standard (scf/hr)	7,444,337	7,669,522	7,825,916	7,646,592
Q <sub>std</sub> Volumetric flow rate, dry standard (dscf/hr)	5,693,704	5,913,611	6,072,448	5,893,254
Q <sub>a</sub> Volumetric flow rate, actual (m <sup>3</sup> /hr)	314,271	324,037	330,902	323,070
Q <sub>s</sub> Volumetric flow rate, standard (m <sup>3</sup> /hr)	210,828	217,205	221,635	216,556
Q <sub>std</sub> Volumetric flow rate, dry standard (dry m <sup>3</sup> /hr)	161,249	167,477	171,975	166,900
Q <sub>std7</sub> Volumetric flow rate, dry std@7%O <sub>2</sub> (dry m <sup>3</sup> /hr)	140,368	143,380	147,231	143,659
Q <sub>s</sub> Volumetric flow rate, normal (Nm <sup>3</sup> /hr)	196,453	202,396	206,523	201,791
Q <sub>std</sub> Volumetric flow rate, dry normal (Nm <sup>3</sup> /hr)	150,255	156,058	160,250	155,521
Q <sub>std7</sub> Volumetric flow rate, dry normal @7%O <sub>2</sub> (Nm <sup>3</sup> /hr)	130,797	133,604	137,192	133,864
<b>Sampling Data</b>				
V <sub>mstd</sub> Volume metered, standard (dscf)	70.3138	72.3661	73.5494	72.0764
%I Isokinetic sampling (%)	99.8589	98.9518	97.9393	98.9167
<b>Laboratory Data</b>				
m <sub>n-1b</sub> Fraction 1B Prorated (µg)	<0.1000	<0.1000	<0.1000	
m <sub>n-2b</sub> Fraction 2B Prorated (µg)	18.9204	21.3248	22.9907	
m <sub>n-3a</sub> Fraction 3A Prorated (µg)	<0.2000	<0.2000	<0.2000	
m <sub>n-3b</sub> Fraction 3B Prorated (µg)	<0.5000	<0.5000	<0.5000	
m <sub>n-3c</sub> Fraction 3C Prorated (µg)	<0.4000	<0.4000	<0.4000	
m <sub>n</sub> Total matter corrected for allowable blanks (µg)	18.9204	21.3248	22.9907	
<b>Mercury Results - Total</b>				
C <sub>sd</sub> Concentration (lb/dscf)	5.9333E-10	6.4977E-10	6.8926E-10	6.4412E-10
C <sub>sd7</sub> Concentration @7% O <sub>2</sub> (lb/dscf)	6.8160E-10	7.5897E-10	8.0510E-10	7.4856E-10
C <sub>sd12</sub> Concentration @12% CO <sub>2</sub> (lb/dscf)	6.7170E-10	7.4973E-10	8.1089E-10	7.4411E-10
C <sub>a</sub> Concentration (lb/acf)	3.0443E-10	3.3583E-10	3.5822E-10	3.3283E-10
C <sub>sd</sub> Concentration (µg/dscm)	9.5014E+00	1.0405E+01	1.1037E+01	1.0315E+01
C <sub>sd7</sub> Concentration @7% O <sub>2</sub> (µg/dscm)	1.0915E+01	1.2154E+01	1.2893E+01	1.1987E+01
C <sub>sd12</sub> Concentration @12% CO <sub>2</sub> (µg/dscm)	1.0756E+01	1.2006E+01	1.2985E+01	1.1916E+01
C <sub>sd</sub> Concentration (mg/dscm)	9.5014E-03	1.0405E-02	1.1037E-02	1.0315E-02
C <sub>sd7</sub> Concentration @7% O <sub>2</sub> (mg/dscm)	1.0915E-02	1.2154E-02	1.2893E-02	1.1987E-02
C <sub>sd12</sub> Concentration @12% CO <sub>2</sub> (mg/dscm)	1.0756E-02	1.2006E-02	1.2985E-02	1.1916E-02
C <sub>a</sub> Concentration (µg/m <sup>3</sup> (actual,wet))	4.8751E+00	5.3778E+00	5.7364E+00	5.3298E+00
C <sub>sd</sub> Concentration (µg/Nm <sup>3</sup> dry)	1.0197E+01	1.1166E+01	1.1845E+01	1.1069E+01
C <sub>sd7</sub> Concentration @7% O <sub>2</sub> (µg/Nm <sup>3</sup> dry)	1.1713E+01	1.3043E+01	1.3836E+01	1.2864E+01
C <sub>sd12</sub> Concentration @12% CO <sub>2</sub> (µg/Nm <sup>3</sup> dry)	1.1543E+01	1.2884E+01	1.3935E+01	1.2788E+01
E <sub>lb/hr</sub> Rate (lb/hr)	3.3783E-03	3.8425E-03	4.1855E-03	3.8021E-03
E <sub>g/s</sub> Rate (g/s)	4.2558E-04	4.8406E-04	5.2727E-04	4.7897E-04
E <sub>T/yr</sub> Rate (Ton/yr)	1.4797E-02	1.6830E-02	1.8332E-02	1.6653E-02
E <sub>Fd</sub> Rate - Fd-based (lb/MMBtu)	9.8078E-06	1.0921E-05	1.1585E-05	1.0771E-05
E <sub>Fc</sub> Rate - Fc-based (lb/MMBtu)	1.0187E-05	1.1371E-05	1.2299E-05	1.1286E-05

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Wheelabrator North Broward, Inc.  
 Clean Air Project No: 10455  
 Unit 1 FF Outlet

**USEPA Method 29  
 Mercury (Hg) Emission Parameters (continued)  
 Separate Front Half Results**

Run No.	1	2	3	Average
Date (2008)	Jun 27	Jun 27	Jun 27	
Start Time (approx.)	09:01	11:36	14:10	
Stop Time (approx.)	11:17	13:50	16:30	

**Mercury Results - Front Half**

C <sub>sd</sub>	Concentration (lb/dscf)	<3.1359E-12	<3.0470E-12	<2.9980E-12	<3.0603E-12
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (lb/dscf)	<3.6024E-12	<3.5591E-12	<3.5018E-12	<3.5545E-12
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (lb/dscf)	<3.5501E-12	<3.5158E-12	<3.5270E-12	<3.5310E-12
C <sub>a</sub>	Concentration (lb/acf)	<1.6090E-12	<1.5748E-12	<1.5581E-12	<1.5807E-12
C <sub>sd</sub>	Concentration (µg/dscm)	<5.0218E-02	<4.8794E-02	<4.8009E-02	<4.9007E-02
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (µg/dscm)	<5.7688E-02	<5.6994E-02	<5.6077E-02	<5.6920E-02
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (µg/dscm)	<5.6850E-02	<5.6300E-02	<5.6481E-02	<5.6544E-02
C <sub>sd</sub>	Concentration (mg/dscm)	<5.0218E-05	<4.8794E-05	<4.8009E-05	<4.9007E-05
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (mg/dscm)	<5.7688E-05	<5.6994E-05	<5.6077E-05	<5.6920E-05
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (mg/dscm)	<5.6850E-05	<5.6300E-05	<5.6481E-05	<5.6544E-05
C <sub>a</sub>	Concentration (µg/m <sup>3</sup> (actual,wet))	<2.5766E-02	<2.5219E-02	<2.4951E-02	<2.5312E-02
C <sub>sd</sub>	Concentration (µg/Nm <sup>3</sup> dry)	<5.3892E-02	<5.2364E-02	<5.1521E-02	<5.2592E-02
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<6.1909E-02	<6.1164E-02	<6.0180E-02	<6.1085E-02
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<6.1010E-02	<6.0420E-02	<6.0613E-02	<6.0681E-02
E <sub>lb/hr</sub>	Rate (lb/hr)	<1.7855E-05	<1.8019E-05	<1.8205E-05	<1.8026E-05
E <sub>g/s</sub>	Rate (g/s)	<2.2493E-06	<2.2699E-06	<2.2934E-06	<2.2709E-06
E <sub>T/yr</sub>	Rate (Ton/yr)	<7.8205E-05	<7.8922E-05	<7.9738E-05	<7.8955E-05
E <sub>Fd</sub>	Rate - Fd-based (lb/MMBtu)	<5.1837E-08	<5.1214E-08	<5.0390E-08	<5.1147E-08
E <sub>Fc</sub>	Rate - Fc-based (lb/MMBtu)	<5.3844E-08	<5.3323E-08	<5.3493E-08	<5.3553E-08

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Wheelabrator North Broward, Inc.  
 Clean Air Project No: 10455  
 Unit 1 FF Outlet

**USEPA Method 29  
 Mercury (Hg) Emission Parameters (continued)  
 Separate Impinger 1-3 Results**

Run No.	1	2	3	Average	
Date (2008)	Jun 27	Jun 27	Jun 27		
Start Time (approx.)	09:01	11:36	14:10		
Stop Time (approx.)	11:17	13:50	16:30		
<b>Mercury Results - Impingers 1-3 Solution</b>					
C <sub>sd</sub>	Concentration (lb/dscf)	5.9333E-10	6.4977E-10	6.8926E-10	<b>6.4412E-10</b>
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (lb/dscf)	6.8160E-10	7.5897E-10	8.0510E-10	<b>7.4856E-10</b>
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (lb/dscf)	6.7170E-10	7.4973E-10	8.1089E-10	<b>7.4411E-10</b>
C <sub>a</sub>	Concentration (lb/acf)	3.0443E-10	3.3583E-10	3.5822E-10	<b>3.3283E-10</b>
C <sub>sd</sub>	Concentration (µg/dscm)	9.5014E+00	1.0405E+01	1.1037E+01	<b>1.0315E+01</b>
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (µg/dscm)	1.0915E+01	1.2154E+01	1.2893E+01	<b>1.1987E+01</b>
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (µg/dscm)	1.0756E+01	1.2006E+01	1.2985E+01	<b>1.1916E+01</b>
C <sub>sd</sub>	Concentration (mg/dscm)	9.5014E-03	1.0405E-02	1.1037E-02	<b>1.0315E-02</b>
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (mg/dscm)	1.0915E-02	1.2154E-02	1.2893E-02	<b>1.1987E-02</b>
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (mg/dscm)	1.0756E-02	1.2006E-02	1.2985E-02	<b>1.1916E-02</b>
C <sub>a</sub>	Concentration (µg/m <sup>3</sup> (actual,wet))	4.8751E+00	5.3778E+00	5.7364E+00	<b>5.3298E+00</b>
C <sub>sd</sub>	Concentration (µg/Nm <sup>3</sup> dry)	1.0197E+01	1.1166E+01	1.1845E+01	<b>1.1069E+01</b>
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (µg/Nm <sup>3</sup> dry)	1.1713E+01	1.3043E+01	1.3836E+01	<b>1.2864E+01</b>
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (µg/Nm <sup>3</sup> dry)	1.1543E+01	1.2884E+01	1.3935E+01	<b>1.2788E+01</b>
E <sub>lb/hr</sub>	Rate (lb/hr)	3.3783E-03	3.8425E-03	4.1855E-03	<b>3.8021E-03</b>
E <sub>g/s</sub>	Rate (g/s)	4.2558E-04	4.8406E-04	5.2727E-04	<b>4.7897E-04</b>
E <sub>T/yr</sub>	Rate (Ton/yr)	1.4797E-02	1.6830E-02	1.8332E-02	<b>1.6653E-02</b>
E <sub>Fd</sub>	Rate - Fd-based (lb/MMBtu)	9.8078E-06	1.0921E-05	1.1585E-05	<b>1.0771E-05</b>
E <sub>Fc</sub>	Rate - Fc-based (lb/MMBtu)	1.0187E-05	1.1371E-05	1.2299E-05	<b>1.1286E-05</b>

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Wheelabrator North Broward, Inc.  
 Clean Air Project No: 10455  
 Unit 1 FF Outlet

**USEPA Method 29  
 Mercury (Hg) Emission Parameters (continued)  
 Separate Impinger 4 Results**

Run No.	1	2	3	Average
Date (2008)	Jun 27	Jun 27	Jun 27	
Start Time (approx.)	09:01	11:36	14:10	
Stop Time (approx.)	11:17	13:50	16:30	

**Mercury Results - Impinger 4 Solution**

C <sub>sd</sub>	Concentration (lb/dscf)	<6.2719E-12	<6.0940E-12	<5.9960E-12	<b>&lt;6.1206E-12</b>
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (lb/dscf)	<7.2049E-12	<7.1182E-12	<7.0037E-12	<b>&lt;7.1089E-12</b>
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (lb/dscf)	<7.1002E-12	<7.0316E-12	<7.0541E-12	<b>&lt;7.0620E-12</b>
C <sub>a</sub>	Concentration (lb/acf)	<3.2180E-12	<3.1497E-12	<3.1162E-12	<b>&lt;3.1613E-12</b>
C <sub>sd</sub>	Concentration (µg/dscm)	<1.0044E-01	<9.7587E-02	<9.6017E-02	<b>&lt;9.8013E-02</b>
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (µg/dscm)	<1.1538E-01	<1.1399E-01	<1.1215E-01	<b>&lt;1.1384E-01</b>
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (µg/dscm)	<1.1370E-01	<1.1260E-01	<1.1296E-01	<b>&lt;1.1309E-01</b>
C <sub>sd</sub>	Concentration (mg/dscm)	<1.0044E-04	<9.7587E-05	<9.6017E-05	<b>&lt;9.8013E-05</b>
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (mg/dscm)	<1.1538E-04	<1.1399E-04	<1.1215E-04	<b>&lt;1.1384E-04</b>
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (mg/dscm)	<1.1370E-04	<1.1260E-04	<1.1296E-04	<b>&lt;1.1309E-04</b>
C <sub>a</sub>	Concentration (µg/m <sup>3</sup> (actual,wet))	<5.1532E-02	<5.0437E-02	<4.9902E-02	<b>&lt;5.0624E-02</b>
C <sub>sd</sub>	Concentration (µg/Nm <sup>3</sup> dry)	<1.0778E-01	<1.0473E-01	<1.0304E-01	<b>&lt;1.0518E-01</b>
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<1.2382E-01	<1.2233E-01	<1.2036E-01	<b>&lt;1.2217E-01</b>
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<1.2202E-01	<1.2084E-01	<1.2123E-01	<b>&lt;1.2136E-01</b>
E <sub>sp/hr</sub>	Rate (lb/hr)	<3.5710E-05	<3.6038E-05	<3.6410E-05	<b>&lt;3.6053E-05</b>
E <sub>g/s</sub>	Rate (g/s)	<4.4986E-06	<4.5399E-06	<4.5868E-06	<b>&lt;4.5418E-06</b>
E <sub>T/yr</sub>	Rate (Ton/yr)	<1.5641E-04	<1.5784E-04	<1.5948E-04	<b>&lt;1.5791E-04</b>
E <sub>Fd</sub>	Rate - Fd-based (lb/MMBtu)	<1.0367E-07	<1.0243E-07	<1.0078E-07	<b>&lt;1.0229E-07</b>
E <sub>Fc</sub>	Rate - Fc-based (lb/MMBtu)	<1.0769E-07	<1.0665E-07	<1.0699E-07	<b>&lt;1.0711E-07</b>

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**USEPA Method 29  
 Mercury (Hg) Emission Parameters (continued)  
 Separate Impinger 5-6 Results**

Run No.	1	2	3	Average
Date (2008)	Jun 27	Jun 27	Jun 27	
Start Time (approx.)	09:01	11:36	14:10	
Stop Time (approx.)	11:17	13:50	16:30	

**Mercury Results - Filtered Permanganate Solution**

C <sub>sd</sub>	Concentration (lb/dscf)	<1.5680E-11	<1.5235E-11	<1.4990E-11	<1.5302E-11
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (lb/dscf)	<1.8012E-11	<1.7796E-11	<1.7509E-11	<1.7772E-11
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (lb/dscf)	<1.7751E-11	<1.7579E-11	<1.7635E-11	<1.7655E-11
C <sub>a</sub>	Concentration (lb/acf)	<8.0451E-12	<7.8742E-12	<7.7905E-12	<7.9033E-12
C <sub>sd</sub>	Concentration (µg/dscm)	<2.5109E-01	<2.4397E-01	<2.4004E-01	<2.4503E-01
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (µg/dscm)	<2.8844E-01	<2.8497E-01	<2.8039E-01	<2.8460E-01
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (µg/dscm)	<2.8425E-01	<2.8150E-01	<2.8240E-01	<2.8272E-01
C <sub>sd</sub>	Concentration (mg/dscm)	<2.5109E-04	<2.4397E-04	<2.4004E-04	<2.4503E-04
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (mg/dscm)	<2.8844E-04	<2.8497E-04	<2.8039E-04	<2.8460E-04
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (mg/dscm)	<2.8425E-04	<2.8150E-04	<2.8240E-04	<2.8272E-04
C <sub>a</sub>	Concentration (µg/m <sup>3</sup> (actual,wet))	<1.2883E-01	<1.2609E-01	<1.2475E-01	<1.2656E-01
C <sub>sd</sub>	Concentration (µg/Nm <sup>3</sup> dry)	<2.6946E-01	<2.6182E-01	<2.5761E-01	<2.6296E-01
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<3.0955E-01	<3.0582E-01	<3.0090E-01	<3.0542E-01
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<3.0505E-01	<3.0210E-01	<3.0307E-01	<3.0341E-01
E <sub>lb/hr</sub>	Rate (lb/hr)	<8.9276E-05	<9.0094E-05	<9.1026E-05	<9.0132E-05
E <sub>g/s</sub>	Rate (g/s)	<1.1247E-05	<1.1350E-05	<1.1467E-05	<1.1354E-05
E <sub>T/yr</sub>	Rate (Ton/yr)	<3.9103E-04	<3.9461E-04	<3.9869E-04	<3.9478E-04
E <sub>Fd</sub>	Rate - Fd-based (lb/MMBtu)	<2.5919E-07	<2.5607E-07	<2.5195E-07	<2.5573E-07
E <sub>Fc</sub>	Rate - Fc-based (lb/MMBtu)	<2.6922E-07	<2.6661E-07	<2.6747E-07	<2.6777E-07

**Mercury Results - HCl Rinse + HCl/MnO2 Precipitate**

C <sub>sd</sub>	Concentration (lb/dscf)	<1.2544E-11	<1.2188E-11	<1.1992E-11	<1.2241E-11
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (lb/dscf)	<1.4410E-11	<1.4236E-11	<1.4007E-11	<1.4218E-11
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (lb/dscf)	<1.4200E-11	<1.4063E-11	<1.4108E-11	<1.4124E-11
C <sub>a</sub>	Concentration (lb/acf)	<6.4361E-12	<6.2993E-12	<6.2324E-12	<6.3226E-12
C <sub>sd</sub>	Concentration (µg/dscm)	<2.0087E-01	<1.9517E-01	<1.9203E-01	<1.9603E-01
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (µg/dscm)	<2.3075E-01	<2.2798E-01	<2.2431E-01	<2.2768E-01
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (µg/dscm)	<2.2740E-01	<2.2520E-01	<2.2592E-01	<2.2617E-01
C <sub>sd</sub>	Concentration (mg/dscm)	<2.0087E-04	<1.9517E-04	<1.9203E-04	<1.9603E-04
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (mg/dscm)	<2.3075E-04	<2.2798E-04	<2.2431E-04	<2.2768E-04
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (mg/dscm)	<2.2740E-04	<2.2520E-04	<2.2592E-04	<2.2617E-04
C <sub>a</sub>	Concentration (µg/m <sup>3</sup> (actual,wet))	<1.0306E-01	<1.0087E-01	<9.9803E-02	<1.0125E-01
C <sub>sd</sub>	Concentration (µg/Nm <sup>3</sup> dry)	<2.1557E-01	<2.0946E-01	<2.0609E-01	<2.1037E-01
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<2.4764E-01	<2.4466E-01	<2.4072E-01	<2.4434E-01
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<2.4404E-01	<2.4168E-01	<2.4245E-01	<2.4272E-01
E <sub>lb/hr</sub>	Rate (lb/hr)	<7.1421E-05	<7.2075E-05	<7.2820E-05	<7.2105E-05
E <sub>g/s</sub>	Rate (g/s)	<8.9973E-06	<9.0798E-06	<9.1736E-06	<9.0836E-06
E <sub>T/yr</sub>	Rate (Ton/yr)	<3.1282E-04	<3.1569E-04	<3.1895E-04	<3.1582E-04
E <sub>Fd</sub>	Rate - Fd-based (lb/MMBtu)	<2.0735E-07	<2.0485E-07	<2.0156E-07	<2.0459E-07
E <sub>Fc</sub>	Rate - Fc-based (lb/MMBtu)	<2.1537E-07	<2.1329E-07	<2.1397E-07	<2.1421E-07

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WHEELABRATOR NORTH BROWARD, INC.  
POMPANO BEACH, FL

Client Reference No: 14800198  
CleanAir Project No: 10455-6

**QA/QC DATA**

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Wheelabrator North Broward, Inc.  
 Clean Air Project No: 10455  
 Unit 1 FF Outlet

### USEPA Method 29 (Trace Metals) QA/QC Results

Run No.	1	2	3
Date (2008)	Jun 27	Jun 27	Jun 27
Start Time (approx.)	09:01	11:36	14:10
Stop Time (approx.)	11:17	13:50	16:30
Total Duration of Test Run (min.)	136	134	140
Net Sampling Time (min.)	125	125	125

#### Sampling System Calibration Summary

	Nozzle ID No:	66-264-1	66-264-1	66-264-1
D <sub>n</sub>	Nozzle Diameter (in):	0.264	0.264	0.264
	Probe ID No:	67-8-15	67-8-15	67-8-15
C <sub>p</sub>	Pitot Coefficient:	0.840	0.840	0.840
	Meter Box ID. No:	66-21	66-21	66-21
Y <sub>d</sub>	Meter Box Yd - Field Sheet	0.9842	0.9842	0.9842
	Meter Box Yd - Database	0.9842	0.9842	0.9842
	Meter Box ΔH@ - Field Sheet	1.8163	1.8163	1.8163
	Meter Box ΔH@ - Database	1.8163	1.8163	1.8163

#### QA/QC

##### Final Leak Check

(a) 4% of Sampling Rate (cfm)	0.0238	0.0248	0.0253
(b) Allowable Rate from Method (cfm)	0.0200	0.0200	0.0200
Allowable Limit - minimum of a and b (cfm)	0.0200	0.0200	0.0200
Actual Final Leak Rate (cfm)	0.0030	0.0020	0.0020

##### Sample Volume

	Minimum Volume Required (dscf)	30.00	30.00	30.00
V <sub>mstd</sub>	Actual Sample Volume (dscf)	70.314	72.366	73.549

##### Alternative Method 5 Post-Test Calibration (EPA ALT-009)

√ΔH <sub>avg</sub>	Average of Square Root of ΔH (in. W.C.)	1.0536	1.0913	1.1114
Y <sub>qa</sub>	Alternative Meter Calibration Factor	0.9863	0.9880	0.9885
	Variation from full-test Y <sub>d</sub> (average ≤ ±5%)	0.2%	0.4%	0.4%

**Average  
0.3%**

##### Mean Isokinetic Sampling Rate Variation

	Minimum Allowable (%)	90	90	90
	Maximum Allowable (%)	110	110	110
%I	Actual Variation (%)	99.86	98.95	97.94

##### Point-by-Point Isokinetic Variation

	Number of points <90%	0	1	0
	Number of points >110%	0	0	0
	Number of points <80%	0	0	0
	Number of points >120%	0	0	0

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# Meter Box Full Test Calibration

Meter Box No: 28-080307-1 (66-21)

Date of Calibration: 8/3/2007

Meter Box  $Y_d$ : 0.9842

Calibration conducted by: M. Vaquero

Meter Box  $\Delta H@$ : 1.8163

Barometric Pressure: 29.40

				Standard Meter Gas Volume (ft <sup>3</sup> )			Meter Box Gas Volume (ft <sup>3</sup> )			Std. Meter Temperature (°F)			Meter Box Temperature (°F)			Time (min.)	Calibration Results	
Q	$\Delta H$	$\Delta P$	$Y_{ds}$	Initial	Final	$V_{ds}$ Net	Initial	Final	$V_d$ Net	In	Out	$T_{ds}$ Avg.	In	$T_o$ Out	$T_d$ Avg.	$\Theta$	$Y_d$	$\Delta H@$
0.954	3.00	-1.90	1.0000	0.000	10.000	10.000	103.446	113.729	10.283	77.0	77.0	77.00	93.0	83.0	88.00	10.12	0.9803	1.7704
0.953	3.00	-1.90	1.0000	0.000	10.000	10.000	113.729	124.011	10.282	77.0	77.0	77.00	93.0	83.0	88.00	10.13	0.9804	1.7739
0.383	0.50	-1.30	1.0000	0.000	5.000	5.000	146.502	151.585	5.083	77.0	77.0	77.00	83.0	82.0	82.50	12.62	0.9893	1.8388
0.382	0.50	-1.30	1.0000	0.000	5.000	5.000	151.585	156.680	5.095	77.0	77.0	77.00	85.0	82.0	83.50	12.63	0.9888	1.8417
0.662	1.50	-1.40	1.0000	0.000	11.000	11.000	163.298	174.599	11.301	77.0	77.0	77.00	89.0	83.0	86.00	16.04	0.9825	1.8378
0.663	1.50	-1.40	1.0000	0.000	10.000	10.000	174.599	184.865	10.266	77.0	77.0	77.00	90.0	83.0	86.50	14.57	0.9842	1.8349
Averages																	0.98425	1.81627

D-4

Nomenclature	Equations
<p><math>P_b</math> Barometric Pressure (in. Hg)</p> <p><math>Q</math> Flow Rate (cfm)</p> <p><math>\Delta H</math> Orifice Pressure differential (in. H<sub>2</sub>O)</p> <p><math>\Delta P</math> Inlet Pressure Differential (in. H<sub>2</sub>O)</p> <p><math>V_d</math> Gas Meter Volume - Dry (ft<sup>3</sup>)</p> <p><math>V_{ds}</math> Standard Meter Volume - Dry (ft<sup>3</sup>)</p> <p><math>T_d</math> Average Meter Box Temperature (°F)</p> <p><math>T_o</math> Outlet Meter Box Temperature (°F)</p> <p><math>T_{ds}</math> Average Standard Meter Temperature (°F)</p> <p><math>Y_d</math> Meter Correction Factor (unitless), <math>Y_i \leq Y_{avg} \pm 0.02</math></p> <p><math>Y_{ds}</math> Standard Meter Correction Factor (unitless)</p> <p><math>\Delta H@</math> Orifice Pressure Differential giving 0.75 cfm of air at 68°F and 29.92 in. Hg (in. H<sub>2</sub>O)</p> <p><math>\Delta H@_i \leq \Delta H@_{avg} \pm 0.2</math></p> <p><math>\Theta</math> Duration of Run (minutes)</p>	$Y_d = (Y_{ds}) \left[ \frac{V_{ds}}{V_d} \right] \left[ \frac{T_d + 460}{T_{ds} + 460} \right] \left[ \frac{P_b + \Delta P / 13.6}{P_b + \Delta H / 13.6} \right]$ $\Delta H@ = \frac{(0.0319)(\Delta H)}{P_b(T_o + 460)} \left[ \frac{(T_{ds} + 460)\Theta}{(V_{ds})(Y_{ds})} \right]^2$ $Q = \frac{17.64(V_{ds})(P_b)}{(T_{ds} + 460)(\Theta)}$

Vacuum Gauge	
Standard (in.Hg)	Gauge (in.Hg)
5.0	5.0
9.9	10.0
14.7	15.0
19.5	20.0
24.4	25.0



## Meter Box Critical Orifice Post-Test Calibration Data

Project No. 10455      Meter No. 66-21      Orifice A-4  
 Location FF Outlet      Meter Yd 0.9842      Orifice K' 0.4923  
 Test Date 6/28/2008      Meter ΔH@ 1.8163      Orifice Cal. Date 10/2/2007  
 Operator C. Slimp      Full Test Cal. Date 8/3/2007

### Leak Checks

**Negative Pressure**  
 No movement of manometer in one-minute  Pass  
**Positive Pressure**  
 No movement of manometer in one-minute  Pass

Barom. Press. (P<sub>b</sub>) 30.05 in. Hg

Important: All leak checks must pass in order for calibration to be valid.

Run	Elapsed Time (minutes)	Meter Volume (dcf)	Meter Temperature		Ambient Temp. - T <sub>amb</sub> (°F)	Orifice ΔH (in. W.C.)	Vacuum (in. Hg)	Net Run Time Θ (minutes)	Net Meter Volume for Run - V <sub>m</sub> (dcf)	Avg Meter Temp. for Run T <sub>m</sub> (°F)	DGM Calibration Factor - Y <sub>i</sub>	Percent Variation - ΔY <sub>i</sub>
			Inlet (°F)	Outlet (°F)								
	0.0	813.200	86	83								
1	5.0	816.44	87	83	90	1.40	17.0	5.0	3.24	84.8	0.9970	0.0%
2	10.0	819.68	88	84	90	1.40	17.0	5.0	3.24	85.5	0.9984	0.1%
3	15.0	822.930	88	84	90	1.40	17.0	5.0	3.25	86.0	0.9962	-0.1%
											Average Y <sub>i</sub>	0.9972
											Cal. Error	1.3%

### Calculations and Specifications

$$Y_i = \frac{K \times P_b \times (T_m + 460) \times \theta}{17.64 \times V_m \times (P_b + \frac{\Delta H}{13.6}) \times \sqrt{T_{amb} + 460}}$$

$$\Delta Y_i = \frac{Y_i - \bar{Y}_i}{\bar{Y}_i} \times 100 \quad \text{Spec.: } \Delta Y_i \leq \pm 2\%$$

$$\text{Cal. Error} = \frac{\bar{Y}_i - Y_d}{Y_d} \times 100 \quad \text{Spec.: } \text{Cal. Error} \leq \pm 5\%$$



# Meter Box - Pyrometer Calibration Sheet

Meter Box No: 28-080307-1 (66-21)

Office: Palatine

Calibrated by: M. Vaquero

Client: Dept 66

Date: 8/3/07

Job No: N/A

Temperature Scale Used: Fahrenheit

Type of Calibration: Full-Test

Calibration Reference Settings (°F)	Pyrometer Reading for each Channel (°F)						
	1 Stack	2 Probe	3 Filter	4 Imp Out	5 Aux	6 DGM In	7 DGM Out
50	48	49	51				
100	98	99	100				
150	148	150	150				
200	198	200	200				
250	248	250	250				
300	298	300	300				
350	348	350	350				
400	398	399	400				
450	448	450	450				
500	498	499	500				
550	548	549	549				
600	598	600	600				

Tolerance =  $\pm 2^{\circ}\text{F}$  difference from reference setting.

## Calibration Reference Information

Reference Used: <u>Omega CL23A</u>	Serial No: <u>T-225950</u>
Calibrated By: <u>JH Metrology</u>	Date Calibrated: <u>10/7/2007</u>
Calibration Report No: <u>R044701</u>	

**SAMPLE PROBE CALIBRATION DATA**

Probe Type: S-Type M-5 I.D. number: 67-8-15

**Thermocouple Calibration**

Reference Type: \_\_\_\_\_ Reference I.D. No: \_\_\_\_\_ Pyrometer I.D. No: \_\_\_\_\_ Degrees: F / C

Point No.	Target Temp.	Reference Temp	Indicated Temp	Temp Difference	% Difference	Specification
1	ice-32°F					%Difference ≤ 1.5
2	ambient-70°F					
3	hot oil-150°F					
4	boiling H <sub>2</sub> O-212°F					
5	hot oil-320°F					

Does assembly meet specifications?  → If "NO" thermocouple must be replaced.

**Geometric Pitot Calibration** *(displays on reverse)*

Is pitot assembly in good repair? YES  NO  If "NO" explain: \_\_\_\_\_  
*If repairs are required, pitot does not meet specification.*



**"S" Pitot**

Measurement		Specification
a1 = <u>1</u>	a2 = <u>2</u>	<10°
b1 = <u>2</u>	b2 = <u>0</u>	<5°
y = <u>0.715</u>	θ = <u>1</u>	Pa + Pb = A
Pa = <u>0.353</u>	Pb = <u>0.358</u>	
A = <u>0.715</u>	Dt = <u>0.250</u>	
Calculations		
z = A sin γ =	<u>0.0125</u>	<0.125"
w = A sin θ =	<u>0.01243</u>	<0.03125"

Does assembly meet specifications?



**Standard Pitot**

Measurement	Specification
Tube O.D. _____	(D)
Static Hole I.D. _____	0.1 x D =
Length, _____	
Tip to Static _____	> 6xD =
Static to Bend _____	> 8xD =

Does assembly meet specifications? YES / NO

If "YES" "S" pitot Cp=0.84; Std pitot Cp=0.99  
 If "NO" wind tunnel calibration is required.

YES / NO

**Wind Tunnel Pitot Calibration**

*All specifications are from EPA-600/9-76-005, section 3.1*

PROBE Cp = 0.84 Calibrated by: Jeff Thomas

Date: 12/26/07

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WHEELABRATOR NORTH BROWARD, INC.  
POMPANO BEACH, FL

Client Reference No: 14800198  
CleanAir Project No: 10455-6

**FIELD DATA**

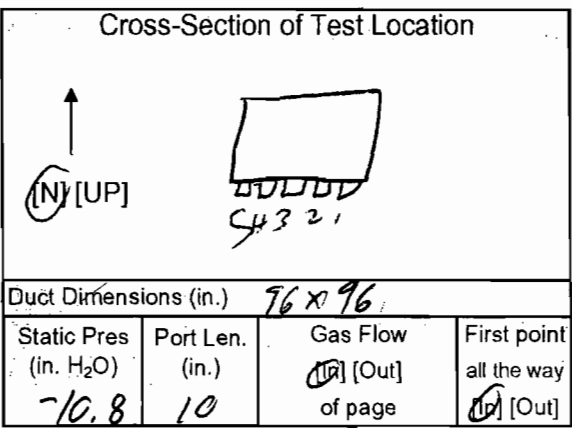
**E**

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TEST LOCATION: FF Outlet      Metals      TESTING METHOD: 29 PAGE 1 OF 2  
 UNIT: 1      RUN: 1  
**FIELD DATA SHEET**

Client <u>Wheelabrator</u>	Project No. <u>10455</u>
Plant <u>N. Browns</u>	Date <u>6-27-08</u>
Meter Operator <u>C. Slomp</u>	
Probe Operator <u>C. Slomp</u>	
Meter Box <u>66-21</u>	Sample Box No. <u>M13</u>
Meter $\gamma_a$ <u>0.9842</u>	Meter $\Delta H_{\theta}$ <u>1.8163</u>
K Factor <u>2.4</u>	Pitot $C_p$ <u>0.84</u>
Leak Rate Before <u>0.0050</u> [Lpm] @ <u>15</u> (in. Hg)	
Leak Rate After <u>0.0030</u> [Lpm] @ <u>10</u> (in. Hg)	
Pitot Leak Check Before: <input checked="" type="checkbox"/> After: Good <input checked="" type="checkbox"/> Bad <input type="checkbox"/>	



Amb. Temp. (°F) <u>90</u>	Bar. Press. <u>30.07</u> [in. Hg] [mbar]
Probe I.D. No. <u>67-8-15</u>	
Liner Material <u>Glass</u>	
Filter No. <u>R1</u>	
Thimble No. <u>—</u>	
Nozzle Diameter <u>0.264</u>	Nozzle I.D. <u>66-264-1</u>
Start Time: <u>0901</u>	Stop Time: <u>11:17</u>

Traverse Point Number	Min/pt Elapsed Time	Velocity Head $\Delta P$ (in. H <sub>2</sub> O)	Orifice Setting $\Delta H$ (in. H <sub>2</sub> O)	Gas Sample Volume $V_m$ Init. Vol. (L)	Stack Temp. $T_s$ (°F)	Probe $T_p$ (°F)	Filter $T_f$ (°F)	Cond. Temp. $T_c$ (°F)	DGM Inlet $T_{min}$ (°F)	DGM Outlet $T_{out}$ (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. (°F)	Notes
						Set Points							
				<u>351.420</u>		<u>250</u>	<u>250</u>						
1-1	5	0.50	1.2	354.57	311	252	252	64	87	85	6	8.5	
2	10	0.46	1.1	357.66	309	253	250	63	88	85	6	9.6	
3	15	0.36	0.86	360.35	304	253	252	64	91	86	6	10.7	
4	20	0.53	1.3	363.44	308	250	248	64	93	86	6	10.5	$\Delta V = 366.755$
5	25	0.60	1.4	<del>366.8754</del>	311	250	251	63	96	87	6.5	9.2	$N.V. = 366.955$
2-1	30	0.45	1.1	369.88	311	250	250	63	95	89	5.5	8.4	$\Delta V = -0.200$
2	35	0.38	0.91	372.78	311	251	250	64	98	89	5.5	7.4	
3	40	0.35	0.84	375.38	310	250	247	63	96	90	5.0	7.9	
4	45	0.55	1.3	378.61	311	249	251	63	98	91	5.9	9.0	
5	50	0.56	1.3	381.760	312	250	251	63	98	92	6.5	7.6	$N.V. = 381.890$
3-1	55	0.45	1.1	384.78	310	251	251	60	96	92	5.5	8.8	$\Delta V = 0.130$
2	60	0.41	0.98	387.59	310	251	250	59	96	92	5	8.3	
		8.167901	13.13		3178				1130	1064			
	Total	<u>17.6547</u>	<u>27.66</u>	<u>74.51</u>	<u>7753</u>				<u>2326</u>	<u>2210</u>			
	Average	<u>0.6822</u>	<u>1.1064</u>		<u>310.12</u>				<u>90.7000</u>				

Sum of square roots  
1.1168

Circle correct bracketed units on data sheet.

QA/QC EA  
 Date 6/23/08

94.72



E-3

TEST LOCATION: FF Outlet  
 UNIT: 1 RUN: 1

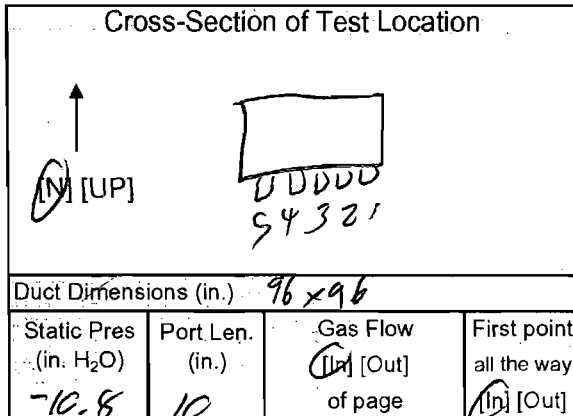
Metals TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 2 OF 2

Client Wheelabrator Project No. 10455  
 Plant N. Browns Date 6-27-08  
 Meter Operator C. Slomp  
 Probe Operator C. Slomp

Meter Box 66-21 Sample Box No. M3  
 Meter Yd 0.9842 Meter  $\Delta H$  1.8163  
 K Factor 2.4 Pitot Cp 0.84

Leak Rate Before [cfm] [Lpm] @ (in. Hg)  
 Leak Rate After [cfm] [Lpm] @ (in. Hg)  
 Pitot Leak Check Before:  After: Good  Bad



Amb. Temp. (°F) 90 Bar. Press. 30.08 [in. Hg] [mbar]  
 Probe I.D. No. 67-A-15  
 Liner Material Glass

Filter No. R1  
 Thimble No. —  
 Nozzle Diameter 0.264 Nozzle I.D. 66-264T

Start Time: Stop Time:

Traverse Point Number	Min/pt 5 Elapsed Time	Velocity Head $\Delta P$ (in. H <sub>2</sub> O)	Orifice Setting $\Delta H$ (in. H <sub>2</sub> O)	Gas Sample Volume $V_m$ Init. Vol. [L]	Stack Temp. $T_s$ (°F)	Probe $T_p$	Filter $T_f$	Cond. Temp. $T_c$ (°F)	DGM Inlet $T_{min}$ (°F)	DGM Outlet $T_{m out}$ (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. $T_t$ (°F)	Notes
						(°F)	(°F)						
3-3	65	0.43	1.0	390.46	312	251	250	58	98	93	5.5	7.8	
4	70	0.52	1.2	393.51	311	250	249	60	98	94	6	7.9	
5	75	0.55	1.3	396.685	308	250	250	61	99	94	6.5	8.3	N.V. = 396.835
4-1	80	0.49	1.2	399.93	311	249	251	62	97	95	6.5	8.2	$\Delta V = 0.150$
2	85	0.44	1.1	403.04	312	250	250	63	99	95	6.5	8.4	
3	90	0.43	1.0	405.99	311	250	250	60	101	95	6	7.8	
4	95	0.53	1.3	409.11	311	250	250	60	100	95	6.5	7.8	
5	100	0.52	1.2	412.265	311	250	250	60	102	96	6.5	7.1	N.V. = 412.830
5-1	105	0.31	0.74	414.87	309	249	251	62	99	97	5	8.0	$\Delta V = 0.165$
2	110	0.37	0.89	417.54	310	250	250	62	100	97	5	7.1	
3	115	0.48	1.2	420.53	311	250	250	63	101	97	6	7.5	
4	120	0.52	1.2	423.53	311	250	250	63	102	98	6	7.4	
5	125	0.52	1.2	426.575	311	249	249	63					
	Total												
	Average												

Sum of square roots.  $\Delta V = 0.645$

Circle correct bracketed units on data sheet.

QA/QC EA  
 Date 6/27/08



E-4

TEST LOCATION: FF Outlet Metals TESTING METHOD: 29 PAGE 1 OF 2  
 UNIT: 1 RUN: 2 FIELD DATA SHEET

Client Wheabrator Project No. 10495  
 Plant N. Broadway Date 6-27-08  
 Meter Operator: C. Slomp  
 Probe Operator: C. Slomp

Meter Box 66-21 Sample Box No. M6  
 Meter  $\gamma_d$ : 0.9842 Meter  $\Delta H_a$ : 1.8163  
 K Factor: 2.4 Pitot  $C_p$ : 0.94  
 Leak Rate Before 0.003 [Lpm] @ 17 (in. Hg)  
 Leak Rate After 1.02 [Lpm] @ 10 (in. Hg)  
 Pitot Leak Check Before:  After: Good  Bad

Cross-Section of Test Location

Duct Dimensions (in.) 9.6 x 9.6

Static Pres (in. H <sub>2</sub> O)	Port Len. (in.)	Gas Flow (in.) [Out]	First point all the way (in.) [Out]
<u>-10.8</u>	<u>10</u>	<u>10</u>	<u>10</u>

Amb. Temp. (°F) 90 Bar. Press. 30.08 [in. Hg] [mbar]  
 Probe I.D. No. 67-8-15  
 Liner Material: Glass

Filter No. R2  
 Thimble No. —  
 Nozzle Diameter 0.264 Nozzle I.D.: 66-264-1

Start Time: 11:36 Stop Time: 13:50

Traverse Point Number	Min/pt Elapsed Time	Velocity Head $\Delta P$ (in. H <sub>2</sub> O)	Orifice Setting $\Delta H$ (in. H <sub>2</sub> O)	Gas Sample Volume $V_m$ Init. Vol. (in.) [L]	Stack Temp. $T_s$ (°F)	Probe $T_p$ (°F)	Filter $T_f$ (°F)	Cond. Temp. $T_c$ (°F)	DGM Inlet $T_{min}$ (°F)	DGM Outlet $T_{m out}$ (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. $T_t$ (°F)	Notes
						Set Points							
1-1	5	0.45	1.1	431.28	310	255	257	64	97	98	5.5	6.8	
2	10	0.49	1.2	434.41	309	255	256	64	98	98	5.5	7.6	
3	15	0.41	0.98	437.25	306+30	250	250	62	100	98	5	8.0	
4	20	0.61	1.5	440.74	312	251	252	60	102	98	6.5	7.8	
5	25	0.70	1.7	444.465	313	250	251	61	103	99	7	7.9	N.V = 444.635
2-1	30	0.42	1.0	447.41	311	250	253	62	99	99	5	6.9	$\Delta V = 0.17$
2	35	0.44	1.1	450.40	311	251	250	61	102	99	5.5	6.8	
3	40	0.48	1.2	457.40	311	251	249	63	103	99	5.5	6.8	
4	45	0.56	1.3	456.69	311	250	249	60	105	99	6	6.9	460.285
5	50	0.61	1.5	460.150	312	249	250	59	105	99	6.5	7.1	N.V = 460.285
3-1	55	0.44	1.1	463.25	310	249	250	61	101	99	5.5	7.3	N.V = 463.25
2	60	0.41	0.98	466.11	311			59	104	99	5	7.6	
		8.4737	14.66	7785	3731				1219	1184			
Total		17.9158	30.01	77470	7725				2549	2486			
Average		0.7038	1.2004	77470	311.0000				100.7000				

Sum of square roots.

Circle correct bracketed units on data sheet.

QA/QC C.S.  
 Date 6-27-08



E-5

TEST LOCATION: FF Outlet  
 UNIT: 1 RUN: 2

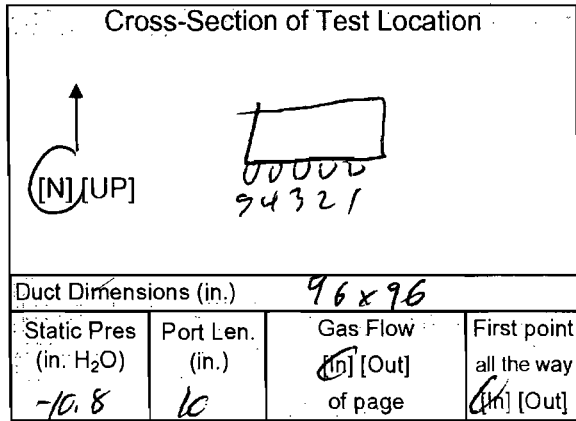
Metals TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 2 OF 2

Client Wheelabrator Project No. 10495  
 Plant N. Browns Date 6-27-08  
 Meter Operator C. Slings  
 Probe Operator C. Slings

Meter Box 66-21 Sample Box No. \_\_\_\_\_  
 Meter Yd 0.9842 Meter ΔH @ 1.8163  
 K Factor 2.4 Pitot Cp 0.94

Leak Rate Before [cfm] [Lpm] @ (in. Hg)  
 Leak Rate After [cfm] [Lpm] @ (in. Hg)  
 Pitot Leak Check Before:  After: Good  Bad



Amb. Temp. (°F) 90 Bar. Press. 30.05 [Hg] [mbar]  
 Probe I.D. No. 67-8-15  
 Liner Material Glass

Filter No. R2  
 Thimble No. \_\_\_\_\_  
 Nozzle Diameter 0.264 Nozzle I.D. \_\_\_\_\_

Start Time: \_\_\_\_\_ Stop Time: \_\_\_\_\_

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. (ft <sup>3</sup> ) [L]	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)		Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>m in</sub> (°F)	DGM Outlet T <sub>m out</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>i</sub> (°F)	Notes
						Set Points	Filter T <sub>f</sub> (°F)						
3-3	65	0.46	1.1	468.94	312	251	250	59	104	100	5	7.0	
4	70	0.56	1.3	472.280	312	250	249	60	104	100	5.5	7.1	
5	75	0.59	1.4	475.645	311	249	249	61	104	101	6.5	7.2	N.V.=475.780
4-1	80	0.38	0.91	478.55	309	248	250	62	100	101	5	7.4	ΔV=0.135
2	85	0.43	1.0	481.47	312	250	250	58	102	100	5.5	7.5	
3	90	0.52	1.2	484.53	311	251	251	58	102	100	5.5	7.5	
4	95	0.65	1.6	487.62	312	251	251	58	103	100	6	7.0	
5	100	0.51	1.2	490.885	309	250	250	60	103	100	5.5	7.1	N.V.=491.050
5-1	105	0.36	0.86	493.76	310	249	249	62	100	100	5	7.3	ΔV=0.165
2	110	0.41	0.98	496.62	312	250	250	62	102	100	5.5	7.3	
3	115	0.45	1.1	499.63	312	251	250	63	102	100	6	7.5	
4	120	0.60	1.4	502.91	311	251	250	63	102	100	6.5	7.0	
5	125	0.53	1.3	506.205	311	250	249	63	102	100	6.5	7.0	
Total													
Average													

Sum of square roots. 0.605

Circle correct bracketed units on data sheet.

QA/QC CS  
 Date 6-27-08



TEST LOCATION: FFG's Fflutlet

Metals

TESTING

METHOD: 29 PAGE 1 OF 2

UNIT: 1

RUN: 3

FIELD DATA SHEET

Client <u>Wheelabrator</u>	Project No. <u>10455</u>
Plant <u>N. Browns</u>	Date <u>6-27-08</u>
Meter Operator: <u>C. Slomp</u>	
Probe Operator: <u>C. Slomp</u>	

Meter Box <u>66-21</u>	Sample Box No. <u>M3</u>
Meter Yd: <u>0.9842</u>	Meter ΔH@: <u>1.863</u>
K Factor: <u>2.4</u>	Pitot Cp: <u>0.84</u>

Leak Rate Before <u>0.002</u> [cm] [Lpm] @ <u>14</u> (in. Hg)
Leak Rate After <u>0.002</u> [cm] [Lpm] @ <u>10</u> (in. Hg)
Pitot Leak Check Before: <input checked="" type="checkbox"/> After: Good <input checked="" type="checkbox"/> Bad <input type="checkbox"/>

Cross-Section of Test Location

Duct Dimensions (in.) 96 x 96

Static Pres (in. H <sub>2</sub> O)	Port Len. (in.)	Gas Flow (ft <sup>3</sup> ) [Out] of page	First point all the way (ft) [Out]
<u>-10.8</u>	<u>10</u>		

Amb. Temp. (°F) <u>90</u>	Bar. Press. <u>30.08</u> [in. Hg] [mbar]
Probe I.D. No. <u>67-8-15</u>	
Liner Material: <u>Glass</u>	

Filter No. <u>R3</u>		
Thimble No. <u>-</u>		
Nozzle Diameter <u>6.264</u>	Nozzle I.D. <u>4-264-1</u>	

Start Time: <u>14:10</u>	Stop Time: <u>16:30</u>
--------------------------	-------------------------

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. [ft <sup>3</sup> ] [L]	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)	Filter T <sub>f</sub> (°F)	Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>min</sub> (°F)	DGM Outlet T <sub>out</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>t</sub> (°F)	Notes
						Set Points							
	<u>5</u>			<u>506.805</u>		<u>250</u>	<u>250</u>						
1-1	<u>5</u>	<u>0.48</u>	<u>1.2</u>	<u>50.00</u>	<u>311</u>	<u>249</u>	<u>245</u>	<u>64</u>	<u>99</u>	<u>100</u>	<u>6.5</u>	<u>9.6</u>	
2	<u>10</u>	<u>0.38</u>	<u>0.91</u>	<u>512.78</u>	<u>309</u>	<u>258</u>	<u>257</u>	<u>64</u>	<u>100</u>	<u>99</u>	<u>5.0</u>	<u>9.5</u>	
3	<u>15</u>	<u>0.46</u>	<u>1.2</u>	<u>515.75</u>	<u>304</u>	<u>254</u>	<u>256</u>	<u>62</u>	<u>100</u>	<u>100</u>	<u>5.5</u>	<u>10.2</u>	
4	<u>20</u>	<u>0.60</u>	<u>1.4</u>	<u>519.08</u>	<u>311</u>	<u>252</u>	<u>246</u>	<u>60</u>	<u>103</u>	<u>100</u>	<u>7</u>	<u>9.8</u>	
5	<u>25</u>	<u>0.60</u>	<u>1.4</u>	<u>522.430</u>	<u>311</u>	<u>250</u>	<u>251</u>	<u>59</u>	<u>105</u>	<u>100</u>	<u>7</u>	<u>10.4</u>	<u>N.V.=522.625</u>
2-1	<u>30</u>	<u>0.40</u>	<u>0.96</u>	<u>525.41</u>	<u>309</u>	<u>249</u>	<u>252</u>	<u>62</u>	<u>102</u>	<u>100</u>	<u>5</u>	<u>10.1</u>	<u>ΔV=0.195</u>
2	<u>35</u>	<u>0.42</u>	<u>1.0</u>	<u>528.28</u>	<u>311</u>	<u>250</u>	<u>251</u>	<u>60</u>	<u>104</u>	<u>100</u>	<u>5.5</u>	<u>9.7</u>	
3	<u>40</u>	<u>0.44</u>	<u>1.0</u>	<u>531.27</u>	<u>311</u>	<u>250</u>	<u>249</u>	<u>60</u>	<u>106</u>	<u>100</u>	<u>6</u>	<u>9.8</u>	
4	<u>45</u>	<u>0.56</u>	<u>1.3</u>	<u>534.43</u>	<u>312</u>	<u>250</u>	<u>250</u>	<u>61</u>	<u>106</u>	<u>101</u>	<u>6.5</u>	<u>9.7</u>	
5	<u>50</u>	<u>0.60</u>	<u>1.4</u>	<u>537.790</u>	<u>311</u>	<u>250</u>	<u>250</u>	<u>61</u>	<u>108</u>	<u>101</u>	<u>7</u>	<u>9.5</u>	<u>N.V.=537.965</u>
3-1	<u>55</u>	<u>0.57</u>	<u>1.3</u>	<u>541.28</u>	<u>310</u>	<u>249</u>	<u>251</u>	<u>62</u>	<u>104</u>	<u>103</u>	<u>7</u>	<u>10.0</u>	<u>ΔV=0.175</u>
2	<u>60</u>	<u>0.45</u>	<u>1.1</u>	<u>544.36</u>	<u>311</u>	<u>250</u>	<u>250</u>	<u>63</u>	<u>102</u>	<u>103</u>	<u>7</u>	<u>10.2</u>	
		<u>8.38882</u>	<u>14.17</u>						<u>103</u>	<u>103</u>			
	Total	<u>(17.977)</u>	<u>(31.07)</u>	<u>79.06</u>		<u>(7790)</u>			<u>(2620)</u>	<u>(2533)</u>			
	Average	<u>(0.7189)</u>	<u>(1.2428)</u>			<u>(311.6000)</u>			<u>(1030600)</u>				

Sum of square roots.

Circle correct bracketed units on data sheet.

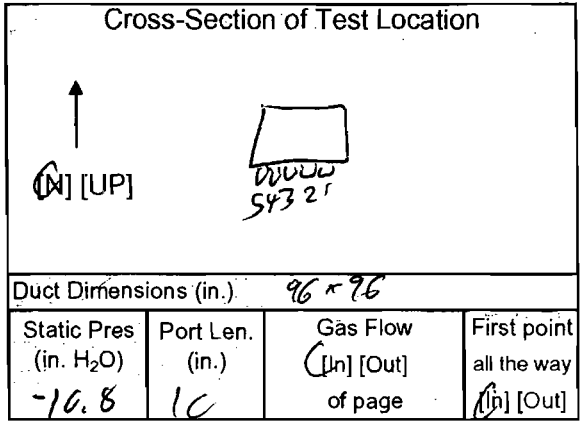
TEST LOCATION: FF Outlet  
 UNIT: 1 RUN: 3

Metals TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 2 OF 2

Client: Wheelabrator Project No. 10455  
 Plant: N. Browns Date: 6-27-08  
 Meter Operator: C. Slings  
 Probe Operator: C. Slings

Meter Box: 66-21 Sample Box No. 173  
 Meter Y: 0.9842 Meter  $\Delta H$ : 1.8163  
 K Factor: 2.4 Pitot C<sub>p</sub>: 0.84  
 Leak Rate Before [cfm] [Lpm] @ (in. Hg)  
 Leak Rate After [cfm] [Lpm] @ (in. Hg)  
 Pitot Leak Check Before:  After: Good  Bad



Amb. Temp. (°F) 90 Bar. Press. 30.08 [in] Hg [mbar]  
 Probe I.D. No. 67-8-15  
 Liner Material

Filter No. R3  
 Thimble No.  
 Nozzle Diameter 0.246 Nozzle I.D. 0.246-1

Start Time: Stop Time:

Traverse Point Number	Min/pt 5 Elapsed Time	Velocity Head $\Delta P$ (in. H <sub>2</sub> O)	Orifice Setting $\Delta H$ (in. H <sub>2</sub> O)	Gas Sample Volume $V_m$		Stack Temp. $T_s$ (°F)	Probe $T_p$ (°F)	Filter $T_f$ (°F)	Cond. Temp. $T_c$ (°F)	DGM Inlet $T_{min}$ (°F)	DGM Outlet $T_{m out}$ (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. $T_t$ (°F)	Notes
				Init. Vol.	[ft <sup>3</sup> ] [L]									
3-3	65	0.46	1.2	547.47	313	250	249	63	108	103	7	9.7		
4	70	0.60	1.4	550.83	312	251	250	62	108	103	7	9.4		
5	79	0.66	1.6	554.450	313	250	249	62	108	103	8	9.1	NV=554.550	
4-1	80	0.42	1.0	557.46	311	249	250	63	109	103	6	9.2	$\Delta V = 0.100$	
2	85	0.42	1.0	560.38	312	250	250	63	106	102	6	9.0		
3	90	0.49	1.2	563.92	312	250	251	63	106	102	6.5	8.9		
4	95	0.60	1.4	566.73	312	250	251	64	106	102	7.0	9.6		
5	100	0.72	1.7	570.460	312	250	250	63	107	101	8.0	9.7	NV=570.870	
5-1	109	0.47	1.1	573.87	313	249	252	64	102	101	6.5	9.8	$\Delta V = 0.410$	
2	110	0.53	1.3	577.01	314	250	251	63	109	101	7	9.8		
3	125	0.60	1.4	580.26	315	250	250	62	104	102	7.5	9.5		
4	120	0.56	1.3	583.52	315	250	250	63	107	101	7.5	9.6		
5	125	0.56	1.3	586.745	315	249	249	64	107	102	7.5	9.7		
	Total								1241	1207				
	Average													

Sum of square roots.

$\Delta V = 0.880$

Circle correct bracketed units on data sheet.

QA/QC CS  
 Date 6/30/08



E-8

# ORSAT READINGS

TEST LOCATION: FF OUTLET

PAGE 1 OF 1

Client:	WHEELABRATOR	Project Number:	10455	$F_o = \frac{20.9 - \%O_2}{\%CO_2}$
Plant:	NORTH BROWARD	Unit:	1	
Orsat ID:	ORSAE #7	Fuel Type:	MSW	Leak Check Passed <input checked="" type="checkbox"/>

Run Number	Method Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> -CO <sub>2</sub>	Percent O <sub>2</sub>	F <sub>o</sub>	Analyst	Analysis	
								Date	Time
1	29	1	10.6	19.4	8.8	1.142	E. DOAK	6/27/08	13 <sup>13</sup>
		2	10.6	19.4	8.8				
		3	10.6	19.4	8.8				
		Avg	10.6		8.8				
2	29	1	10.4	19.4	9.0	1.144	E. DOAK	6/27/08	13 <sup>50</sup>
		2	10.4	19.4	9.0				
		3	10.4	19.4	9.0				
		Avg	10.4		9.0				
3	29	1	10.2	19.2	9.0	1.167	E. DOAK	6/27/08	16 <sup>57</sup>
		2	10.2	19.2	9.0				
		3	10.2	19.2	9.0				
		Avg	10.2		9.0				
		1							
		2							
		3							
		Avg							
		1							
		2							
		3							
		Avg							
		1							
		2							
		3							
		Avg							

Repeat the analysis procedure until the results of any three analyses differ by no more than 0.2 percent by volume. Average the three acceptable values and report the results to the nearest 0.1 percent. Calculate F<sub>o</sub> to verify result.

Acceptable ranges for F<sub>o</sub>:

Coal:	Anthracite and lignite	1.016-1.130	Gas:	Natural	1.600-1.836
	Bituminous	1.083-1.230		Propane	1.434-1.586
Oil:	Distillate	1.260-1.413		Butane	1.405-1.553
	Residual	1.210-1.370	Wood:		1.000-1.120

# Impinger Weight Sheet

Client: <b>WHEELABRATOR</b>	Unit Name / Location: <b>U1 / FF OUTLET</b>
Plant: <b>NORTH BROWNS</b>	Job No.: <b>10455</b> Method: <b>29</b>

Run No.: <b>1</b>	Filter Type: <b>QUARTZ</b>	Sample Box No.: <b>66 M3</b>
Date: <b>6/27/08</b>	Lot No.: <b>NA</b>	pH: <b>NA</b>
Analyst: <b>E. DOAK</b>	Filter No.: <b>NA</b>	Rinse: <b>NA</b>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	EMPTY	848.7	523.0	325.7	
Impinger 2	100 ml 5% HNO <sub>3</sub> / 10% H <sub>2</sub> O <sub>2</sub>	718.4	621.1	97.3	QA/QC Date
Impinger 3	100 ml 5% HNO <sub>3</sub> / 10% H <sub>2</sub> O <sub>2</sub>	635.3	617.5	17.8	
Impinger 4	EMPTY	495.1	492.8	2.3	
Impinger 5	100 ml 4% KMnO <sub>4</sub> / 10% H <sub>2</sub> SO <sub>4</sub>	609.8	608.8	1.0	Total Weight (gm)
Impinger 6	100 ml 4% KMnO <sub>4</sub> / 10% H <sub>2</sub> SO <sub>4</sub>	598.6	599.7	-1.1	443.0
Impinger 7	SILICA GEL	812.0	795.7	16.3	459.3

Run No.: <b>2</b>	Filter Type: <b>QUARTZ</b>	Sample Box No.: <b>66 M6</b>
Date: <b>6/27/08</b>	Lot No.: <b>NA</b>	pH: <b>NA</b>
Analyst: <b>E. DOAK</b>	Filter No.: <b>NA</b>	Rinse: <b>NA</b>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	EMPTY	894.0	522.6	371.4	
Impinger 2	100 ml 5% HNO <sub>3</sub> / 10% H <sub>2</sub> O <sub>2</sub>	672.2	607.3	64.9	QA/QC Date
Impinger 3	100 ml 5% HNO <sub>3</sub> / 10% H <sub>2</sub> O <sub>2</sub>	603.1	597.7	5.4	
Impinger 4	EMPTY	508.6	507.8	0.8	
Impinger 5	100 ml 4% KMnO <sub>4</sub> / 10% H <sub>2</sub> SO <sub>4</sub>	586.0	584.9	1.1	Total Weight (gm)
Impinger 6	100 ml 4% KMnO <sub>4</sub> / 10% H <sub>2</sub> SO <sub>4</sub>	607.3	607.7	-0.4	443.2
Impinger 7	SILICA GEL	755.8	742.5	13.3	456.5

Run No.: <b>3</b>	Filter Type: <b>QUARTZ</b>	Sample Box No.: <b>66 M3</b>
Date: <b>6/27/08</b>	Lot No.: <b>NA</b>	pH: <b>NA</b>
Analyst: <b>EA</b>	Filter No.: <b>NA</b>	Rinse: <b>NA</b>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	EMPTY	835.9	523.0	312.9	
Impinger 2	100 ml 5% HNO <sub>3</sub> / 10% H <sub>2</sub> O <sub>2</sub>	725.4	617.0	<del>58</del> 118 + 108.4	QA/QC Date
Impinger 3	100 ml 5% HNO <sub>3</sub> / 10% H <sub>2</sub> O <sub>2</sub>	630.5	619.0	11.5	
Impinger 4	EMPTY	494.7	493.2	1.5	
Impinger 5	100 ml 4% KMnO <sub>4</sub> / 10% H <sub>2</sub> SO <sub>4</sub>	603.5	602.4	1.1	Total Weight (gm)
Impinger 6	100 ml 4% KMnO <sub>4</sub> / 10% H <sub>2</sub> SO <sub>4</sub>	603.1	603.0	0.1	<del>4350.45</del> 0.58
Impinger 7	SILICA GEL	828.5	812.3	<del>58</del> 14.2 / 6.2	<del>451.24</del> 59.258



TEST LOCATION: FF Outlet Metals TESTING METHOD: 29 PAGE 1 OF 2

UNIT: 1 RUN: 4

**FIELD DATA SHEET**

Client <u>Wheelabrator</u>	Project No. <u>10459</u>
Plant <u>N. Browns</u>	Date <u>6-28-08</u>
Meter Operator <u>C. Slomp</u>	
Probe Operator <u>C. Slomp</u>	

Meter Box <u>66-21</u>	Sample Box No. <u>M6</u>
Meter $Y_a$ <u>0.9842</u>	Meter $\Delta H_a$ <u>1.8163</u>
K Factor <u>2.4</u>	Pitot $C_p$ <u>0.84</u>
Leak Rate Before <u>0.003</u> [cfm] [Lpm] @ <u>15</u> (in. Hg)	
Leak Rate After <u>0.102</u> [cfm] [Lpm] @ <u>12</u> (in. Hg)	
Pitot Leak Check Before: <input checked="" type="checkbox"/> After: Good <input checked="" type="checkbox"/> Bad <input type="checkbox"/>	

Cross-Section of Test Location

Duct Dimensions (in.) 96x96

Static Pres (in. H <sub>2</sub> O)	Port Len. (in.)	Gas Flow (in) [Out] of page	First point all the way (in) [Out]
<u>-11.5</u>	<u>10</u>		

Amb. Temp. (°F) <u>85</u>	Bar. Press. <u>30.05</u> (in. Hg) [mbar]
Probe I.D. No. <u>67-8-15</u>	
Liner Material <u>Glass</u>	

Filter No. <u>R4</u>		
Thimble No. <u>-</u>		
Nozzle Diameter <u>0.264</u>	Nozzle I.D.	<u>65-264-2</u>

Start Time: <u>06:43</u>	Stop Time: <u>08:58</u>
--------------------------	-------------------------

Traverse Point Number	Min/pt Elapsed Time	Velocity Head $\Delta P$ (in. H <sub>2</sub> O)	Orifice Setting $\Delta H$ (in. H <sub>2</sub> O)	Gas Sample Volume $V_m$ Init. Vol. [L]	Stack Temp. $T_s$ (°F)	Probe $T_p$ (°F)		Filter $T_f$ (°F)	Cond. Temp. $T_c$ (°F)	DGM Inlet $T_{min}$ (°F)	DGM Outlet $T_{mout}$ (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. $T_t$ (°F)	Notes
						Set Points								
1-1	5	0.52	1.2	587.155	310	250	250	250	64	82	82	5.5	9.1	
2	10	0.50	1.2	593.23	310	254	255	255	60	83	83	5.5	9.0	
3	15	0.38	0.91	599.94	297	254	252	252	58	86	83	5	9.0	
4	20	0.61	1.5	599.33	312	250	247	247	58	86	83	7	9.0	
5	25	0.63	1.5	602.785	311	250	248	248	60	88	84	7	9.3	N.V.=603.000
2-1	30	0.42	1.0	609.87	309	250	252	252	62	86	84	5.5	9.0	$\Delta V=0.215$
2	35	0.44	1.1	608.71	309	251	251	251	61	90	85	5.5	9.0	
3	40	0.42	1.0	611.57	309	251	250	250	60	90	85	5.5	9.2	
4	45	0.48	1.2	614.63	309	250	248	248	58	92	86	5.5	9.0	
5	50	0.55	1.3	617.795	310	250	250	250	59	93	86	6.0	8.9	N.V.=617.955
3-1	55	0.38	0.91	620.67	309	249	250	250	60	90	87	5	9.0	$\Delta V=0.160$
2	60	0.38	0.91	623.40	310	250	249	249	59	91	87			
		0.46204	13.73		3709					1059	1015			
Total		16.6044	26.892	72.965	7736					2278	2176			
Average		0.6642	1.0756		309.44					89.0800				

Sum of Square roots. 0.6642

Circle correct bracketed units on data sheet.



E-11

TEST LOCATION: FF Outlet  
 UNIT: 1 RUN: 4

Metals TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 2 OF 2

Client Wheelabrator Project No. 10455  
 Plant N. Browns Date 6-28-08  
 Meter Operator C. Slimg  
 Probe Operator C. Slimg

Meter Box 66-21 Sample Box No. M6  
 Meter Yd 0.9842 Meter  $\Delta H$  @ 1.8163  
 K Factor 2.4 Pitot C<sub>p</sub> 0.84

Leak Rate Before [cfm] [Lpm] @ (in. Hg)  
 Leak Rate After: [cfm] [Lpm] @ (in. Hg)  
 Pitot Leak Check Before:  After: Good  Bad

Cross-Section of Test Location

Duct Dimensions (in.) 96 x 96

Static Pres (in. H <sub>2</sub> O)	Port Len. (in.)	Gas Flow (In) [Out] of page	First point all the way (In) [Out]
<u>-11.5</u>	<u>10</u>		<u>0</u> [Out]

Amb. Temp. (°F) 85 Bar. Press: 30.05 (in. Hg) [mbar]  
 Probe I.D. No. 67-8-15  
 Liner Material Glass

Filter No. R4  
 Thimble No. -  
 Nozzle Diameter 0.264 Nozzle I.D. 66-264-2

Start Time: Stop Time:

Traverse Point Number	Min/pt S Elapsed Time	Velocity Head $\Delta P$ (in. H <sub>2</sub> O)	Orifice Setting $\Delta H$ (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. [ft <sup>3</sup> ] [L]	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)	Filter T <sub>f</sub> (°F)	Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>min</sub> (°F)	DGM Outlet T <sub>max</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>t</sub> (°F)	Notes
						Set Points							
3-3	65	0.44	1.1	626.30	310	250	250	60	93	87	5.5	9.8	
4	70	0.50	1.2	629.24	311	251	250	60	94	88	5.5	9.5	
5	75	0.53	1.3	632.410	310	250	250	58	94	88	6	9.4	W.V. = 632.560
4-1	80	0.38	0.91	635.25	309	248	251	61	91	89	5	9.3	$\Delta V = 0.150$
2	85	0.32	0.77	637.73	310	250	251	58	93	89	5	9.1	
3	90	0.35	0.84	640.31	310	250	250	59	93	89	5	9.0	
4	95	0.45	1.1	643.33	310	250	250	59	94	89	6	8.9	
5	100	0.48	1.2	646.410	310	250	250	62	96	90	6	8.9	W.V. = 646.545
5-1	105	0.36	0.74	649.00	309	249	250	62	92	90	5	8.9	$\Delta V = 0.135$
2	110	0.41	0.98	651.81	310	250	250	62	94	90	5.5	9.0	
3	115	0.40	0.96	654.62	310	250	250	61	95	91	5.5	9.0	
4	120	0.46	1.2	657.69	311	250	250	61	95	90	6	9.0	
9	129	0.36	0.86	660.380	311	250	250	62	95	91			
Total													
Average													

Sum of square roots.

$\Delta V_1 = 0.660$

Circle correct bracketed units on data sheet.

QA/QC CS  
 Date 6-28

TEST LOCATION: FF Outlet  
 UNIT: 1 RUN: 5

Metals TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 1 OF 2

Client Wheelabrator Project No. 10455  
 Plant N. Browns Date 6-28-06  
 Meter Operator C. Slomp  
 Probe Operator C. Slomp

Meter Box 66-21 Sample Box No. M3  
 Meter Y<sub>d</sub> 0.9842 Meter ΔH<sub>@</sub> 1.8163  
 K Factor 2.4 Pitot C<sub>p</sub> 0.84

Leak Rate Before 6.009 [Lpm] @ 15 (in. Hg)  
 Leak Rate After 1.004 [Lpm] @ 10 (in. Hg)  
 Pitot Leak Check Before:  After: Good  Bad

Cross-Section of Test Location

Static Pres (in. H<sub>2</sub>O) -1.5 Port Len. (in.) 10 Gas Flow [UP] [Out] of page First point all the way [UP] [Out]

Duct Dimensions (in.) 96 x 96

Amb. Temp. (°F) 90 Bar. Press. 30.05 [in Hg] [mbar]  
 Probe I.D. No. 67-8-15  
 Liner Material Glass

Filter No. R5  
 Thimble No. —  
 Nozzle Diameter 0.264 Nozzle I.D. 66-264-2

Start Time: 09:15 Stop Time: 11:30

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. [L]	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)	Filter T <sub>f</sub> (°F)	Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>min</sub> (°F)	DGM Outlet T <sub>max</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>t</sub> (°F)	Notes
						Set Points							
1-1	5	0.47	1.1	660.785	310	295	292	64	92	92	5.5	9.0	
2	10	0.44	1.1	666.78	310	297	299	64	94	91	5.5	9.1	
3	15	0.30	0.72	669.58	290	293	290	63	95	91	5.0	9.0	
4	20	0.50	1.2	672.69	310	290	291	63	96	92	6.0	8.9	
5	25	0.54	1.3	675.50	311	290	249	63	97	92	6.5	9.0	NV=676.145
2-1	30	0.45	1.1	679.23	309	290	291	63	94	93	6	9.0	NV=0.195
2	35	0.44	1.1	682.28	311	291	290	62	98	93	6	8.9	
3	40	0.41	0.98	685.15	310	291	248	62	99	94	6	9.0	
4	45	0.46	1.1	688.16	311	290	290	62	99	94	6	8.9	
5	50	0.50	1.2	691.280	310	249	290	62	100	95	6	9.0	NV=691.420
3-1	55	0.35	0.84	694.03	310	290	291	63	97	95	5	8.9	NV=0.140
2	60	0.40	0.96	696.69	310	290	290	62	98	95	5	9.1	
		7.92243	12.7		3702				1159	1117			
	Total	16.6603	26.96	74.445	7750				2473	2388			
	Average	0.16664	1.0784		310.0000				97.2200				

Sum of square roots.

Circle correct bracketed units on data sheet.

QA/QC CS  
 Date 6-28-06



E-13

TEST LOCATION: FF Outlet  
 UNIT: 1 RUN: 5

Metals TESTING  
 FIELD DATA SHEET

METHOD: 29 PAGE 2 OF 2

Client Wheelabrator Project No. 10455  
 Plant N. Browns Date 6-28-08  
 Meter Operator C. Slomp  
 Probe Operator C. Slomp

Meter Box 66-21 Sample Box No. \_\_\_\_\_  
 Meter  $\gamma$  0.9842 Meter  $\Delta H$  @ 1.8163  
 K Factor 2.4 Pitot  $C_p$  0.89  
 Leak Rate Before [cfm] [Lpm] @ (in. Hg) \_\_\_\_\_  
 Leak Rate After [cfm] [Lpm] @ (in. Hg) \_\_\_\_\_  
 Pitot Leak Check Before:  After: Good  Bad

Cross-Section of Test Location

Duct Dimensions (in.) 96x26

Static Pres (in. H <sub>2</sub> O)	Port Len. (in.)	Gas Flow (IN) [Out] of page	First point all the way (IN) [Out]
<u>-11.5</u>	<u>10</u>		

Amb. Temp. (°F) 90 Bar. Press. 30.05 [in. Hg] [mbar]  
 Probe I.D. No. 67-8-15  
 Liner Material Glass

Filter No. RS  
 Thimble No. \_\_\_\_\_  
 Nozzle Diameter 0.64 Nozzle I.D. 66-264-2

Start Time: \_\_\_\_\_ Stop Time: \_\_\_\_\_

Traverse Point Number	Min/pt Elapsed Time	Velocity Head $\Delta P$ (in. H <sub>2</sub> O)	Orifice Setting $\Delta H$ (in. H <sub>2</sub> O)	Gas Sample Volume $V_m$ Init. Vol. (ft <sup>3</sup> ) [L]	Stack Temp. $T_s$ (°F)	Probe $T_p$ (°F)	Filter $T_f$ (°F)	Cond. Temp. $T_c$ (°F)	DGM Inlet $T_{min}$ (°F)	DGM Outlet $T_{out}$ (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. $T_t$ (°F)	Notes
						Set Points							
3-3	65	0.42	1.0	699.53	312	251	251	62	99	96	5.5	8.9	
4	76	0.48	1.2	702.61	312	250	249	62	100	96	6	9.0	
5	75	0.54	1.3	705.935	311	249	249	63	102	96	6.5	8.9	N.V. = 706.35
4-1	80	0.41	0.98	708.88	310	251	250	64	99	97	5.5	9.0	$\Delta V = 0.100$
2	85	0.39	0.94	711.65	312	251	250	63	102	98	5.5	8.9	
3	90	0.47	1.1	714.63	312	251	250	62	101	98	6	9.1	
4	95	0.59	1.4	718.07	312	250	250	63	102	98	6.5	9.4	
5	100	0.54	1.3	721.420	312	249	249	61	103	98	6.9	9.7	N.V. = 721.538
5-1	105	0.30	0.72	723.96	311	249	250	62	99	99	5	9.6	$v = 0.110$
2	110	0.34	0.82	726.52	310	249	250	63	101	99	5	9.3	
3	115	0.45	1.1	729.49	311	251	250	62	102	98	6	9.8	
4	120	0.50	1.2	732.63	311	250	250	61	102	99	6.5	9.4	
5	125	0.49	1.2	735.775	312	248	249	60	102	99		9.5	
	Total	*											
	Average												

Sum of square roots.

Circle correct bracketed units on data sheet.

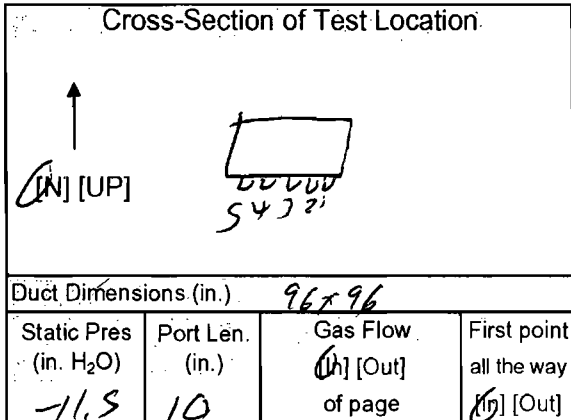
$\Delta V_t = 0.545$

QA/QC CS  
 Date 6-28-08

TEST LOCATION: FF Outlet Metals TESTING METHOD: 29 PAGE 1 OF 2  
 UNIT: 1 RUN: 6 FIELD DATA SHEET

Client Wheelabrator Project No. 10455  
 Plant N. Browns Date 6-28-07  
 Meter Operator C. Slimp  
 Probe Operator C. Slimp

Meter Box 66-21 Sample Box No. M6  
 Meter Yd. 0.9842 Meter ΔH@ 1.8163  
 K Factor 2.4 Pitot Cp 0.84  
 Leak Rate Before 0.003 [cfm] [Lpm] @ 15 (in. Hg)  
 Leak Rate After 0.002 [cfm] [Lpm] @ 10 (in. Hg)  
 Pitot Leak Check Before:  After: Good  Bad



Amb. Temp. (°F) 90 Bar. Press. 30.05 (in. Hg) [mbar]  
 Probe I.D. No. 67-8-15  
 Liner Material Glass

Filter No. R6  
 Thimble No. —  
 Nozzle Diameter 0.246 Nozzle I.D. 66-264-2  
0.264

Start Time: 11:48 Stop Time: 14:02

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. (ft <sup>3</sup> ) [L]	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> Filter T <sub>f</sub> (°F)		Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>min</sub> (°F)	DGM Outlet T <sub>out</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>f</sub> (°F)	Notes
						Set Points	Set Points						
1-1	5	0.50	1.2	737.280	311	250	251	63	98	98	5.5	10.4	
2	10	0.45	1.1	743.48	312	252	254	63	100	99	5.5	10.0	
3	15	0.30	0.72	745.99	296	250	250	60	103	99	5.5	10.6	
4	20	0.50	1.2	749.06	311	250	249	60	101	99	5.5	11.0	
5	25	0.65	1.6	752.625	311	251	252	60	103	99	5.5	10.9	N.V.=752.860
2-16cs	30	0.48	1.2	755.93	311	250	254	62	100	99	5.5	10.9	ΔV=0.235
27cs	35	0.55	1.3	559.30	312	251	250	60	102	99	6.0	11.0	
38cs	40	0.36	0.86	761.95	310	250	251	61	103	99	5.0	12.1	
44cs	45	0.49	1.2	764.99	311	250	250	62	103	99	6	10.4	
5	50	0.45	1.1	768.095	310	249	246	62	103	99	6	7.5	N.V.=768.360
3-1	55	0.35	0.84	771.07	310	249	250	63	100	99	5	10.0	ΔV=0.265
2	60	0.48	1.2	774.15	311	250	250	61	102	100	6	10.6	
		8.12867	13.52		3716				1218	1188			
Total		16.6972	22.35	74.520	7753				2558	2496	2496		
Average		0.6679	1.0940		310.1200				101.0800				

Sum of square roots.

Circle correct bracketed units on data sheet.



E-15

TEST LOCATION: FF Outlet  
 UNIT: 1 RUN: 6

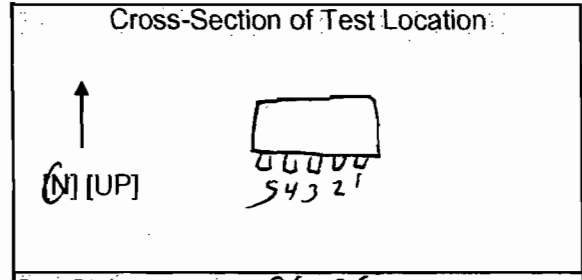
Metals TESTING  
 FIELD DATA SHEET

METHOD: 29 PAGE 2 OF 2

Client Wheelabrator Project No. 10455  
 Plant N. Browns Date 6-28-08  
 Meter Operator C. Slomp  
 Probe Operator C. Slomp

Meter Box 66-21 Sample Box No. M6  
 Meter  $V_d$  0.9842 Meter  $\Delta H$  @ 1.8163  
 K Factor 2.4 Pitot  $C_p$  0.84

Leak Rate Before [cfm] [Lpm] @ (in. Hg)  
 Leak Rate After [cfm] [Lpm] @ (in. Hg)  
 Pitot Leak Check Before:  After: Good  Bad



Amb. Temp. (°F) 90 Bar. Press. 30.05 (in. Hg) [mbar]  
 Probe I.D. No. 67-8-15  
 Liner Material Glass

Filter No. R6  
 Thimble No. —  
 Nozzle Diameter 2.64 Nozzle I.D. 86-264-2

Duct Dimensions (in.) 96 x 96  
 Static Pres (in. H<sub>2</sub>O) -11.5 Port Len. (in.) 10 Gas Flow (in) [Out] (N) [Out] First point all the way (N) [Out] of page

Start Time: Stop Time:

Traverse Point Number	Min/pt Elapsed Time	Velocity Head $\Delta P$ (in. H <sub>2</sub> O)	Orifice Setting $\Delta H$ (in. H <sub>2</sub> O)	Gas Sample Volume $V_m$ Init. Vol. (L)	Stack Temp. $T_s$ (°F)	Probe $T_p$ (°F)		Cond. Temp. $T_c$ (°F)	DGM Inlet $T_{min}$ (°F)	DGM Outlet $T_{out}$ (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. $T_t$ (°F)	Notes
						Set Points	Set Points						
3-3	65	0.50	1.2	777.27	313	291	290	58	104	99	6.0	10.7	
4	70	0.53	1.3	780.54	312	291	292	58	104	100	6.0	10.9	
5	75	0.56	1.3	783.825	311	249	246	59	104	100	6.0	11.0	N.Y. = 784.00
4-1	80	0.34	0.82	786.59	309	252	249	62	103	100	5	10.1	$\Delta V = 0.185$
2	85	0.33	0.79	789.12	310	250	250	62	102	101	5	7.6	
3	90	0.41	0.98	791.87	310	250	249	62	102	101	5	8.4	
4	95	0.50	1.2	795.02	310	251	250	62	104	101	5.5	8.6	
5	100	0.48	1.2	798.160	311	250	249	62	105	101	6	8.5	N.Y. = 798.360
5-1	105	0.30	0.72	800.78	309	249	250	63	102	101	5	9.5	$\Delta V = 0.200$
2	110	0.34	0.82	803.21	310	250	250	61	102	101	5.0	9.3	
3	115	0.45	1.1	806.32	310	250	249	60	102	101	6.0	9.2	
4	120	0.48	1.2	809.51	311	250	250	60	103	101	6.5	9.3	
5	125	0.48	1.2	812.685	311	251	250	60	103	101			
	Total												
	Average												

Sum of square roots. 0.885 =  $\Delta V$

Circle correct bracketed units on data sheet.

QA/QC SB  
 Date 7/1/08



E-16

# Impinger Weight Sheet

Client: <b>WHEELABRATOR</b>	Unit Name / Location: <b>U1 / FF OUTLET</b>
Plant: <b>NORTH BROWARD</b>	Job No: <b>10456</b> Method: <b>29</b>

Run No: <b>4</b>	Filter Type: <b>QUARTZ</b>	Sample Box No: <b>66 M6</b>
Date: <b>6/28/08</b>	Lot No: <b>NA</b>	pH: <b>NA</b>
Analyst: <b>E. DOAK</b>	Filter No: <b>NA</b>	Rinse: <b>NA</b>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	EMPTY	882.2	522.5	359.7	
Impinger 2	100ml 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	698.8	610.5	88.3	QA/QC Date
Impinger 3	100ml 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	610.9	600.8	10.1	
Impinger 4	EMPTY	509.1	507.8	1.3	
Impinger 5	100ml 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	585.3	582.7	2.6	Total Weight (gm)
Impinger 6	100ml 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	617.5	617.2	0.3	462.3
Impinger 7	SILICA GEL	755.1	738.8	16.3	478.6

Run No: <b>5</b>	Filter Type: <b>QUARTZ</b>	Sample Box No: <b>66 M3</b>
Date: <b>6/28/08</b>	Lot No: <b>NA</b>	pH: <b>NA</b>
Analyst: <b>E. DOAK</b>	Filter No: <b>NA</b>	Rinse: <b>NA</b>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	EMPTY	862.6	523.0	339.6	
Impinger 2	100ml 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	720.7	620.8	99.9	QA/QC Date
Impinger 3	100ml 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	633.6	624.8	8.8	
Impinger 4	EMPTY	493.2	492.8	0.4	
Impinger 5	100ml 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	610.4	610.0	0.4	Total Weight (gm)
Impinger 6	100ml 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	600.2	601.0	-0.8	448.3
Impinger 7	SILICA GEL	846.3	834.2	12.1	460.4

Run No: <b>6</b>	Filter Type: <b>QUARTZ</b>	Sample Box No: <b>66 M6</b>
Date: <b>6/28/08</b>	Lot No: <b>NA</b>	pH: <b>NA</b>
Analyst: <b>E. DOAK</b>	Filter No: <b>NA</b>	Rinse: <b>NA</b>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	EMPTY	862.7	522.6	340.1	
Impinger 2	100ml 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	700.7	608.4	92.3	QA/QC Date
Impinger 3	100ml 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	610.8	605.3	5.5	
Impinger 4	EMPTY	508.8	508.2	0.6	
Impinger 5	100ml 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	587.9	586.3	1.6	Total Weight (gm)
Impinger 6	100ml 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	611.9	612.0	-0.1	440.0
Impinger 7	SILICA GEL	767.8	755.1	12.7	452.7

# Impinger Weight Sheet

Client: <b>WHEELABRATOR</b>	Unit Name / Location: <b>UI / FF OUTLET</b>
Plant: <b>NORTH BROWARA</b>	Job No: <b>10455</b> Method: <b>29</b>

Run No: <b>FIELD BLANK</b>	Filter Type: <b>QUARTZ</b>	Sample Box No: <b>66 M6</b>
Date: <b>6/27/08</b>	Lot No: <b>NA</b>	pH: <b>NA</b>
Analyst: <b>E. DOAK</b>	Filter No: <b>NA</b>	Rinse: <b>NA</b>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	EMPTY	522.4	EA <del>742</del> 522.4	0.0	
Impinger 2	100 ml 5% HNO <sub>3</sub> / 10% H <sub>2</sub> O <sub>2</sub>	605.2	605.3	-0.1	QA/QC
Impinger 3	100 ml 5% HNO <sub>3</sub> / 10% H <sub>2</sub> O <sub>2</sub>	596.4	596.4	0.0	Date
Impinger 4	EMPTY	507.8	507.8	0.0	
Impinger 5	100 ml 1% KMnO <sub>4</sub> / 10% H <sub>2</sub> SO <sub>4</sub>	582.3	582.4	-0.1	Total Weight (gm)
Impinger 6	100 ml 1% KMnO <sub>4</sub> / 10% H <sub>2</sub> SO <sub>4</sub>	604.1	604.1	0.0	-0.2
Impinger 7	EMPTY	742.4	742.4	0.0	-0.2

Run No:	Filter Type:	Sample Box No:
Date:	Lot No:	pH:
Analyst:	Filter No:	Rinse:

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1					
Impinger 2					QA/QC
Impinger 3					Date
Impinger 4					
Impinger 5					Total Weight (gm)
Impinger 6					
Impinger 7					

Run No:	Filter Type:	Sample Box No:
Date:	Lot No:	pH:
Analyst:	Filter No:	Rinse:

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1					
Impinger 2					QA/QC
Impinger 3					Date
Impinger 4					
Impinger 5					Total Weight (gm)
Impinger 6					
Impinger 7					



# ORSAT READINGS

TEST LOCATION: FF Outlet

PAGE 1 OF 1

Client: <u>WHEELABRATOR</u>	Project Number: <u>10455</u>	$Fo = \frac{20.9 - \%O_2}{\%CO_2}$
Plant: <u>NORTH BROWARD</u>	Unit: <u>1</u>	
Orsat ID: <u>ORSAT # 7</u>	Fuel Type: <u>MSW</u>	Leak Check Passed <input checked="" type="checkbox"/>

Run Number	Method Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Fo	Analyst	Analysis	
								Date	Time
4	29	1	11.0	19.6	8.6	1.118	E. DOAK	6/28/08	10:52
		2	11.0	19.6	8.6				
		3	11.0	19.6	8.6				
		Avg	11.0		8.6				
5	29	1	10.9	19.6	8.7	1.119	E. DOAK	6/28/08	12:24
		2	11.0	19.6	8.6				
		3	10.9	19.6	8.7				
		Avg	10.93		8.67				
6	29	1	10.6	19.2	8.6	1.160	E. DOAK	6/28/08	14:53
		2	10.6	19.2	8.6				
		3	10.6	19.2	8.6				
		Avg	10.6		8.6				
		1							
		2							
		3							
		Avg							
		1							
		2							
		3							
		Avg							
		1							
		2							
		3							
		Avg							

Repeat the analysis procedure until the results of any three analyses differ by no more than 0.2 percent by volume. Average the three acceptable values and report the results to the nearest 0.1 percent. Calculate Fo to verify result.

Acceptable ranges for Fo:

Coal:	Anthracite and lignite	1.016-1.130	Gas:	Natural	1.600-1.836
	Bituminous	1.083-1.230		Propane	1.434-1.586
Oil:	Distillate	1.260-1.413		Butane	1.405-1.553
	Residual	1.210-1.370	Wood:		1.000-1.120

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WHEELABRATOR NORTH BROWARD, INC.  
POMPANO BEACH, FL

Client Reference No: 14800198  
CleanAir Project No: 10455-6

**FIELD DATA PRINTOUTS**

F

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**Field Data Printout**

**Test Method: USEPA Method 29**  
**Analyte: Trace Metals**

Location: Unit 1 FF Outlet  
 Test Run: 1  
 Client: Wheelabrator North Broward, Inc.  
 Project No: 10455  
 Source Area (ft<sup>2</sup>): 64.00000  
 Meter Operator: C. Slimp 558  
 Probe Operator: C. Slimp 558  
 Test Date: 6/27/08  
 Start Time: 09:01  
 Stop Time: 11:17  
 Leak Rate Before: 0.005 cfm @ 15 "Hg  
 Leak Rate After: 0.003 cfm @ 10 "Hg

Bar. Press. (in. Hg): 30.07  
 Static P: -10.8  
 O<sub>2</sub> (dry volume %): 8.80  
 CO<sub>2</sub> (dry volume %): 10.60  
 N<sub>2</sub>+CO (dry volume %): 80.60

Nozzle ID No: 66-264-1  
 Nozzle Diameter (D<sub>n</sub>): 0.264  
 Probe ID No: 67-8-15  
 Pitot C<sub>p</sub>: 0.84  
 Pitot Leak Check:  Pass  Fail

H<sub>2</sub>O (condensate, ml or gm): 443.0  
 H<sub>2</sub>O (silica, g): 16.3  
 Actual Moisture (%): 23.52

Meter Box ID No: 66-21  
 Meter ΔH@: 1.81630  
 Meter Y<sub>s</sub>: 0.98420

Traverse Point	Run Time 5.0 min/read	Pitot ΔP <sub>s</sub> (in. H <sub>2</sub> O)	Sample ΔH (in. H <sub>2</sub> O)	Metered (dcf)	Stack T <sub>s</sub> (°F)	Dry Gas Meter		√ΔP <sub>s</sub> (calculated) (√in. H <sub>2</sub> O)	Volume (calculated) (ft <sup>3</sup> )	Isokinetics (calculated) (%)
						T <sub>m-in</sub> (°F)	T <sub>m-out</sub> (°F)			
1-01	0.0	0.50	1.20	351.420	311	87	85	0.71	3.15	103.5
1-02	5.0	0.46	1.10	354.570	309	88	85	0.68	3.09	105.6
1-03	10.0	0.36	0.86	360.350	304	91	86	0.60	2.69	103.2
1-04	15.0	0.53	1.30	363.440	308	93	86	0.73	3.09	97.8
1-05	20.0	0.60	1.40	366.755	311	96	87	0.77	3.32	98.5
LEAK CHECK	25.0			366.955						
2-01	25.0	0.45	1.10	369.880	311	95	89	0.67	2.93	100.2
2-02	30.0	0.38	0.91	372.780	311	98	89	0.62	2.90	107.8
2-03	35.0	0.35	0.84	375.380	310	96	90	0.59	2.60	100.7
2-04	40.0	0.55	1.30	378.610	311	96	91	0.74	3.23	99.9
2-05	45.0	0.56	1.30	381.760	312	98	92	0.75	3.15	96.3
LEAK CHECK	50.0			381.890						
3-01	50.0	0.45	1.10	384.780	310	96	92	0.67	2.89	98.6
3-02	55.0	0.41	0.98	387.590	310	96	92	0.64	2.81	100.4
3-03	60.0	0.43	1.00	390.460	312	98	93	0.66	2.87	100.0
3-04	65.0	0.52	1.20	393.510	311	98	94	0.72	3.05	96.5
3-05	70.0	0.55	1.30	396.685	308	99	94	0.74	3.18	97.5
LEAK CHECK	75.0			396.835						
4-01	75.0	0.49	1.20	399.930	311	97	95	0.70	3.10	100.9
4-02	80.0	0.44	1.10	403.040	312	99	95	0.66	3.11	106.9
4-03	85.0	0.43	1.00	405.990	311	101	95	0.66	2.95	102.3
4-04	90.0	0.53	1.30	409.110	311	100	95	0.73	3.12	97.6
4-05	95.0	0.52	1.20	412.265	311	102	96	0.72	3.15	99.3
LEAK CHECK	100.0			412.430						
5-01	100.0	0.31	0.74	414.870	305	99	97	0.56	2.44	99.2
5-02	105.0	0.37	0.89	417.540	310	100	97	0.61	2.67	99.6
5-03	110.0	0.48	1.20	420.530	311	101	97	0.69	2.99	98.0
5-04	115.0	0.52	1.20	423.550	311	102	98	0.72	3.02	94.9
5-05	120.0	0.52	1.20	426.575	311	102	98	0.72	3.02	95.1
Final	125.0		1.11680	74.51000	310.12000	94.72000		0.68219	74.51000	

25 points sampled  
 QC-Check: Field Averages  
 Sq.Rt.ΔP: 0.6822 1.1168 74.5100 310.1200 94.7200  
 Avg. OK  Avg. OK  Avg. OK  Avg. OK  Avg. OK

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 P

**Field Data Printout**

**Test Method: USEPA Method 29**  
**Analyte: Trace Metals**

Location: Unit 1 FF Outlet  
 Test Run: 2  
 Client: Wheelabrator North Broward, Inc.  
 Project No: 10455  
 Source Area (ft<sup>2</sup>): 64.00000  
 Meter Operator: C. Slimp 558  
 Probe Operator: C. Slimp 558  
 Test Date: 6/27/08  
 Start Time: 11:36  
 Stop Time: 13:50  
 Leak Rate Before: 0.003 cfm @ 17 "Hg  
 Leak Rate After: 0.002 cfm @ 10 "Hg

Bar. Press. (in. Hg): 30.08  
 Static P: -10.8  
 O<sub>2</sub> (dry volume %): 9.00  
 CO<sub>2</sub> (dry volume %): 10.40  
 N<sub>2</sub>+CO (dry volume %): 80.60

Nozzle ID No: 66-264-1  
 Nozzle Diameter (D<sub>n</sub>): 0.264  
 Probe ID No: 67-8-15  
 Pitot C<sub>p</sub>: 0.84  
 Pitot Leak Check:  Pass  Fail

H<sub>2</sub>O (condensate, ml or gm): 443.2  
 H<sub>2</sub>O (silica, g): 13.3  
 Actual Moisture (%): 22.89

Meter Box ID No: 66-21  
 Meter ΔH@: 1.81630  
 Meter Y<sub>a</sub>: 0.98420

Traverse Point	Run Time 5.0 min/read	Pitot ΔP <sub>s</sub> (in. H <sub>2</sub> O)	Sample ΔH (in. H <sub>2</sub> O)	Metered (dcf)	Stack T <sub>s</sub> (°F)	Dry Gas Meter		√ΔP <sub>s</sub> (calculated) (√in. H <sub>2</sub> O)	Volume (calculated) (ft <sup>3</sup> )	Isokinetics (calculated) (%)
						T <sub>m-in</sub> (°F)	T <sub>m-out</sub> (°F)			
	0.0			428.130						
1-01	5.0	0.45	1.10	431.280	310	97	98	0.67	3.15	106.0
1-02	10.0	0.49	1.20	434.410	309	98	98	0.70	3.13	100.9
1-03	15.0	0.41	0.98	437.280	310	100	98	0.64	2.87	100.9
1-04	20.0	0.61	1.50	440.740	312	102	98	0.78	3.46	99.8
1-05	25.0	0.70	1.70	444.465	313	103	99	0.84	3.72	100.3
LEAK CHECK	25.0			444.635						
2-01	30.0	0.43	1.00	447.440	311	99	99	0.66	2.81	96.4
2-02	35.0	0.44	1.10	450.400	311	102	99	0.66	2.96	100.3
2-03	40.0	0.48	1.20	453.400	311	103	99	0.69	3.00	97.3
2-04	45.0	0.56	1.30	456.690	311	105	99	0.75	3.29	98.6
2-05	50.0	0.61	1.50	460.150	312	105	99	0.78	3.46	99.5
LEAK CHECK	50.0			460.285						
3-01	55.0	0.44	1.10	463.250	310	101	99	0.66	2.96	100.5
3-02	60.0	0.41	0.98	466.110	311	104	99	0.64	2.86	100.2
3-03	65.0	0.46	1.10	468.940	312	104	100	0.68	2.83	93.6
3-04	70.0	0.56	1.30	472.280	312	104	100	0.75	3.34	100.2
3-05	75.0	0.59	1.40	475.645	311	104	101	0.77	3.37	98.2
LEAK CHECK	75.0			475.780						
4-01	80.0	0.38	0.91	478.550	309	100	101	0.62	2.77	100.8
4-02	85.0	0.43	1.00	481.430	312	102	100	0.66	2.88	98.7
4-03	90.0	0.52	1.20	484.530	311	102	100	0.72	3.10	96.6
4-04	95.0	0.65	1.60	487.620	312	103	100	0.81	3.09	86.2*
4-05	100.0	0.51	1.20	490.885	309	103	100	0.71	3.26	102.5
LEAK CHECK	100.0			491.050						
5-01	105.0	0.36	0.86	493.760	310	100	100	0.60	2.71	101.5
5-02	110.0	0.41	0.98	496.620	312	102	100	0.64	2.86	100.3
5-03	115.0	0.45	1.10	499.630	312	102	100	0.67	3.01	100.8
5-04	120.0	0.60	1.40	502.910	311	102	100	0.77	3.28	95.2
5-05	125.0	0.53	1.30	506.205	311	102	100	0.73	3.29	101.7
Final	125.0		1.20040	77.47000	311.00000	100.70000		0.70383	77.47000	

25 points sampled  
 QC-Check: Field Averages

Sq.Rt.ΔP	0.7038	1.2004	77.4700	311.0000	100.7000
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Avg. OK    Avg. OK    Avg. OK    Avg. OK    Avg. OK

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**Field Data Printout**

**Test Method:** USEPA Method 29  
**Analyte:** Trace Metals

Location: Unit 1 FF Outlet  
 Test Run: 3  
 Client: Wheelabrator North Broward, Inc.  
 Project No: 10455  
 Source Area (ft<sup>2</sup>): 64.00000  
 Meter Operator: C. Slimp 558  
 Probe Operator: C. Slimp 558  
 Test Date: 6/27/08  
 Start Time: 14:10  
 Stop Time: 16:30  
 Leak Rate Before: 0.003 cfm @ 14 "Hg  
 Leak Rate After: 0.002 cfm @ 20 "Hg

Bar. Press. (in. Hg): 30.08  
 Static P: -10.8  
 O<sub>2</sub> (dry volume %): 9.00  
 CO<sub>2</sub> (dry volume %): 10.20  
 N<sub>2</sub>+CO (dry volume %): 80.80

Nozzle ID No: 66-264-1  
 Nozzle Diameter (D<sub>n</sub>): 0.264  
 Probe ID No: 67-8-15  
 Pitot C<sub>p</sub>: 0.84  
 Pitot Leak Check:  Pass  Fail

H<sub>2</sub>O (condensate, ml or gm): 435.0  
 H<sub>2</sub>O (silica, g): 16.2  
 Actual Moisture (%): 22.41

Meter Box ID No: 66-21  
 Meter ΔH@: 1.81630  
 Meter Y<sub>d</sub>: 0.98420

Traverse Point	Run Time 5.0 min/read	Pitot ΔP <sub>s</sub> (in. H <sub>2</sub> O)	Sample ΔH (in. H <sub>2</sub> O)	Metered (dcf)	Stack T <sub>e</sub> (°F)	Dry Gas Meter		√ΔP <sub>s</sub> (calculated) (√in. H <sub>2</sub> O)	Volume (calculated) (ft <sup>3</sup> )	Isokinetics (calculated) (%)
						T <sub>m-in</sub> (°F)	T <sub>m-out</sub> (°F)			
	0.0			506.805						
1-01	5.0	0.48	1.20	510.000	311	99	100	0.69	3.19	103.3
1-02	10.0	0.38	0.91	512.780	309	100	99	0.62	2.78	100.8
1-03	15.0	0.46	1.10	515.750	304	102	100	0.68	2.97	97.3
1-04	20.0	0.60	1.40	519.080	311	103	100	0.77	3.33	96.0
1-05	25.0	0.60	1.40	522.430	311	105	100	0.77	3.35	96.4
LEAK CHECK	25.0			522.625						
2-01	30.0	0.40	0.96	525.410	309	102	100	0.63	2.78	98.2
2-02	35.0	0.42	1.00	528.280	311	104	100	0.65	2.87	98.7
2-03	40.0	0.44	1.10	531.270	311	106	100	0.66	2.99	100.3
2-04	45.0	0.54	1.30	534.430	312	106	101	0.73	3.16	95.7
2-05	50.0	0.60	1.40	537.790	311	108	101	0.77	3.36	96.3
LEAK CHECK	50.0			537.965						
3-01	55.0	0.53	1.30	541.280	310	104	103	0.73	3.31	101.2
3-02	60.0	0.45	1.10	544.360	311	102	103	0.67	3.08	102.3
3-03	65.0	0.48	1.20	547.470	313	108	103	0.69	3.11	99.6
3-04	70.0	0.60	1.40	550.830	312	108	103	0.77	3.36	96.2
3-05	75.0	0.66	1.60	554.450	313	108	103	0.81	3.62	99.0
LEAK CHECK	75.0			554.550						
4-01	80.0	0.42	1.00	557.460	311	105	103	0.65	2.91	99.7
4-02	85.0	0.42	1.00	560.380	312	106	102	0.65	2.92	100.1
4-03	90.0	0.49	1.20	563.520	312	106	102	0.70	3.14	99.7
4-04	95.0	0.60	1.40	566.730	312	106	102	0.77	3.21	92.2
4-05	100.0	0.72	1.70	570.460	312	107	101	0.85	3.73	97.8
LEAK CHECK	100.0			570.870						
5-01	105.0	0.47	1.10	573.870	313	102	101	0.69	3.00	97.8
5-02	110.0	0.53	1.30	577.010	314	105	101	0.73	3.14	96.2
5-03	115.0	0.60	1.40	580.260	315	104	102	0.77	3.25	93.7
5-04	120.0	0.56	1.30	583.520	315	107	101	0.75	3.26	97.1
5-05	125.0	0.56	1.30	586.745	315	107	102	0.75	3.23	95.9
Final	125.0		1.24280	79.06000	311.60000		103.06000	0.71891	79.06000	

25 points sampled  
 QC-Check: Field Averages

Sq.Rt.ΔP	0.7189	1.2428	79.0600	311.6000	103.0600
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Avg. OK     Avg. OK     Avg. OK     Avg. OK     Avg. OK

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**USEPA Method 3 Laboratory Data**

Location: Unit 1 FF Outlet  
 Client: Wheelabrator North Broward, Inc.  
 Project No: 10455  
 Method: EPA Method 3  
 Fuel Type: Municipal Waste  
 F<sub>o</sub> for Fuel: 1.03 to 1.3

**Test Method:** USEPA Method 29  
**Analyte:** Trace Metals

Analyst: E. Doak  
 Analyst Emp No: 349

Run Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Percent N <sub>2</sub>	Dry Mol. Weight	F <sub>o</sub>	Method of Analysis: Orsat
1	1	10.6	19.4	8.8	80.6	30.05	1.14151	All measurements in spec. <input checked="" type="checkbox"/> F <sub>o</sub> value within expected range.
	2	10.6	19.4	8.8	80.6	30.05		
	3	10.6	19.4	8.8	80.6	30.05		
Avg.		10.60000		8.80000	80.60000	30.05		
CEM or Other Avg:								

Run Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Percent N <sub>2</sub>	Dry Mol. Weight	F <sub>o</sub>	Method of Analysis: Orsat
2	1	10.4	19.4	9.0	80.6	30.02	1.14423	All measurements in spec. <input checked="" type="checkbox"/> F <sub>o</sub> value within expected range.
	2	10.4	19.4	9.0	80.6	30.02		
	3	10.4	19.4	9.0	80.6	30.02		
Avg.		10.40000		9.00000	80.60000	30.02		
CEM or Other Avg:								

Run Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Percent N <sub>2</sub>	Dry Mol. Weight	F <sub>o</sub>	Method of Analysis: Orsat
3	1	10.2	19.2	9.0	80.8	29.99	1.16667	All measurements in spec. <input checked="" type="checkbox"/> F <sub>o</sub> value within expected range.
	2	10.2	19.2	9.0	80.8	29.99		
	3	10.2	19.2	9.0	80.8	29.99		
Avg.		10.20000		9.00000	80.80000	29.99		
CEM or Other Avg:								

Run Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Percent N <sub>2</sub>	Dry Mol. Weight	F <sub>o</sub>	Method of Analysis:
	1							
	2							
	3							
Avg.								
CEM or Other Avg:								<input type="checkbox"/> F <sub>o</sub> value within expected range.

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**USEPA Method 4 Laboratory Data**

Location: Unit 1 FF Outlet  
 Client: Wheelabrator North Broward, Inc.  
 Project No: 10455

**Test Method: USEPA Method 29**  
**Analyte: Trace Metals**  
 Analyst: E. Doak  
 Analyst Emp No: 349

Test Run: 1

	Contents	Gross (gm)	Tare (gm)	Net (gm)		
Impinger 1	Empty	848.7	523.0	325.7		
Impinger 2	5%HNO3/10%H2O2	718.4	621.1	97.3		
Impinger 3	5%HNO3/10%H2O2	635.3	617.5	17.8		
Impinger 4	Empty	495.1	492.8	2.3		
Impinger 5	4%KMnO4/10%H2SO4	609.8	608.8	1.0		
Impinger 6	4%KMnO4/10%H2SO4	598.6	599.7	-1.1	443.0 Liquid (gm)	Field Data Check
Impinger 7	Silica Gel	812.0	795.7	16.3	0.0 less rinse (gm)	
Impinger 8					443.0 Net Liquid (gm)	443.0 <input checked="" type="checkbox"/> QA/QC OK
					+ 16.3 Silica Gel (gm)	16.3 <input checked="" type="checkbox"/> QA/QC OK
					459.3 Total Vlc (gm)	459.3 <input checked="" type="checkbox"/> QA/QC OK

Rinse: \_\_\_\_\_ (ml or gm)

Test Run: 2

	Contents	Gross (gm)	Tare (gm)	Net (gm)		
Impinger 1	Empty	894.0	522.6	371.4		
Impinger 2	5%HNO3/10%H2O2	672.2	607.3	64.9		
Impinger 3	5%HNO3/10%H2O2	603.1	597.7	5.4		
Impinger 4	Empty	508.6	507.8	0.8		
Impinger 5	4%KMnO4/10%H2SO4	586.0	584.9	1.1		
Impinger 6	4%KMnO4/10%H2SO4	607.3	607.7	-0.4	443.2 Liquid (gm)	Field Data Check
Impinger 7	Silica Gel	755.8	742.5	13.3	0.0 less rinse (gm)	
Impinger 8					443.2 Net Liquid (gm)	443.2 <input checked="" type="checkbox"/> QA/QC OK
					+ 13.3 Silica Gel (gm)	13.3 <input checked="" type="checkbox"/> QA/QC OK
					456.5 Total Vlc (gm)	456.5 <input checked="" type="checkbox"/> QA/QC OK

Rinse: \_\_\_\_\_ (ml or gm)

Test Run: 3

	Contents	Gross (gm)	Tare (gm)	Net (gm)		
Impinger 1	Empty	835.4	523.0	312.4		
Impinger 2	5%HNO3/10%H2O2	725.4	617.0	108.4		
Impinger 3	5%HNO3/10%H2O2	630.5	619.0	11.5		
Impinger 4	Empty	494.7	493.2	1.5		
Impinger 5	4%KMnO4/10%H2SO4	603.5	602.4	1.1		
Impinger 6	4%KMnO4/10%H2SO4	603.1	603.0	0.1	435.0 Liquid (gm)	Field Data Check
Impinger 7	Silica Gel	828.5	812.3	16.2	0.0 less rinse (gm)	
Impinger 8					435.0 Net Liquid (gm)	435.0 <input checked="" type="checkbox"/> QA/QC OK
					+ 16.2 Silica Gel (gm)	16.2 <input checked="" type="checkbox"/> QA/QC OK
					451.2 Total Vlc (gm)	451.2 <input checked="" type="checkbox"/> QA/QC OK

Rinse: \_\_\_\_\_ (ml or gm)

Test Run: \_\_\_\_\_

	Contents	Gross (gm)	Tare (gm)	Net (gm)		
Impinger 1	Empty					
Impinger 2	5%HNO3/10%H2O2					
Impinger 3	5%HNO3/10%H2O2					
Impinger 4	Empty					
Impinger 5	4%KMnO4/10%H2SO4					
Impinger 6	4%KMnO4/10%H2SO4					
Impinger 7	Silica Gel					
Impinger 8						

Rinse: \_\_\_\_\_ (ml or gm)

	Field Data Check
Liquid (gm)	
less rinse (gm)	
Net Liquid (gm)	<input type="checkbox"/> QA/QC OK
Silica Gel (gm)	<input type="checkbox"/> QA/QC OK
Total Vlc (gm)	<input type="checkbox"/> QA/QC OK

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WHEELABRATOR NORTH BROWARD, INC.  
POMPANO BEACH, FL

Client Reference No: 14800198  
CleanAir Project No: 10455-6

**LABORATORY DATA**

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Wheelabrator North Broward, Inc.  
 Clean Air Project No: 10455  
 Unit 1 FF Outlet

**USEPA Method 29  
 Mercury (Hg) Laboratory Parameters**

**Blank Analysis**

m <sub>1b-B</sub>	Fraction 1B Blank (µg)	<0.1000
m <sub>2b-B</sub>	Fraction 2B Blank (µg)	<0.2000
m <sub>3a-B</sub>	Fraction 3A Blank (µg)	<0.2000
m <sub>3b-B</sub>	Fraction 3B Blank (µg)	<0.5000
m <sub>3c-B</sub>	Fraction 3C Blank (µg)	<0.4000
m <sub>total-B</sub>	Total Blank Amount (µg)	<1.4000

Run No.	1	2	3
Date (2008)	Jun 27	Jun 27	Jun 27
Start Time (approx.)	09:01	11:36	14:10
Stop Time (approx.)	11:17	13:50	16:30

**Sample Analysis**

m <sub>1b-S</sub>	Fraction 1B Sample (µg)	<0.1000	<0.1000	<0.1000
m <sub>2b-S</sub>	Fraction 2B Sample (µg)	18.9204	21.3248	22.9907
m <sub>3a-S</sub>	Fraction 3A Sample (µg)	<0.2000	<0.2000	<0.2000
m <sub>3b-S</sub>	Fraction 3B Sample (µg)	<0.5000	<0.5000	<0.5000
m <sub>3c-S</sub>	Fraction 3C Sample (µg)	<0.4000	<0.4000	<0.4000
m <sub>total-S</sub>	Total Sample Amount (µg)	18.9204	21.3248	22.9907

**Allowable Blank**

m <sub>T-B-allow</sub>	Total Allowable Blank (µg)	0.0000	0.0000	0.0000
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**Sample Corrected for Blank**

m <sub>n</sub>	Total Sample Amount (µg)	18.9204	21.3248	22.9907
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**Sample Corrected for Blank**

m <sub>n-1b</sub>	Fraction 1B (µg)	<0.1000	<0.1000	<0.1000
m <sub>n-2b</sub>	Fraction 2B (µg)	18.9204	21.3248	22.9907
m <sub>n-3a</sub>	Fraction 3A (µg)	<0.2000	<0.2000	<0.2000
m <sub>n-3b</sub>	Fraction 3B (µg)	<0.5000	<0.5000	<0.5000
m <sub>n-3c</sub>	Fraction 3C (µg)	<0.4000	<0.4000	<0.4000

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# **Clean Air Engineering, Inc.**

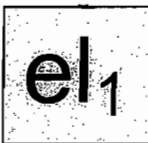
500 West Wood Street  
Palatine, IL 60067

Project Number: 10455

Mercury

EPA Method 29 Analysis

Analytical Report  
11024



Element One, Inc.  
5022-C Wrightsville Av., Wilmington, NC 28403  
910-793-0128 FAX: 910-792-6853 e1lab@e1lab.com

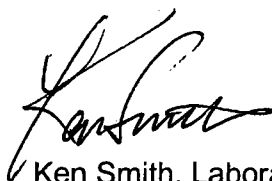
The following data for Analytical Report 11024  
has been reviewed for completeness, accuracy,  
adherence to method protocol,  
and compliance with quality assurance guidelines.

Review by:



Daphne Woodman, Chemist  
July 15, 2008

Report Reviewed and Finalized By:



Ken Smith, Laboratory Director  
July 15, 2008

**elementOne**

11024 Clean Air M29 Report Packet  
Page 2 of 25



# SUMMARY OF RESULTS

**elementOne**

11024 Clean Air M29 Report Packet

Page 3 of 25

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## Summary of Analysis

### Unit 1 North - Summary of Method 29 Mercury Analysis

Run Number	Average Total Catch, $\mu\text{g}$	Front half $\mu\text{g}$	$\text{H}_2\text{O}_2$ / $\text{HNO}_3$ $\mu\text{g}$	Empty Impinger $\mu\text{g}$	$\text{KMnO}_4$ $\mu\text{g}$	$\text{HCl}$ $\mu\text{g}$
U1 FF Outlet N R1 #1	18.9	< 0.1	18.9	< 0.2	< 0.5	< 0.4
#2		< 0.1	18.9	< 0.2	< 0.5	< 0.4
U1 FF Outlet N R2 #1	21.3	< 0.1	21.3	< 0.2	< 0.5	< 0.4
#2		< 0.1	21.3	< 0.2	< 0.5	< 0.4
U1 FF Outlet N R3 #1	25.0	< 0.1	25.3	< 0.2	< 0.5	< 0.4
#2		< 0.1	24.7	< 0.2	< 0.5	< 0.4
N Field Blank #1	< 0.5	< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
#2		< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
N Reagent Blank #1	< 0.5	< 0.1	< 0.2	< 0.2	< 0.5	< 0.4
#2		< 0.1	< 0.2	< 0.2	< 0.5	< 0.4

### Unit 1 South - Summary of Method 29 Mercury Analysis

Run Number	Average Total Catch, $\mu\text{g}$	Front half $\mu\text{g}$	$\text{H}_2\text{O}_2$ / $\text{HNO}_3$ $\mu\text{g}$	Empty Impinger $\mu\text{g}$	$\text{KMnO}_4$ $\mu\text{g}$	$\text{HCl}$ $\mu\text{g}$
U1 FF Outlet S R4 #1	18.5	< 0.1	18.5	< 0.2	< 0.5	< 0.4
#2		< 0.1	18.5	< 0.2	< 0.5	< 0.4
U1 FF Outlet S R5 #1	16.5	< 0.1	16.5	< 0.2	< 0.5	< 0.4
#2		< 0.1	16.5	< 0.2	< 0.5	< 0.4
U1 FF Outlet S R6 #1	19.3	< 0.1	19.3	< 0.2	< 0.5	< 0.4
#2		< 0.1	19.3	< 0.2	< 0.5	< 0.4
S Field Blank #1	< 0.5	< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
#2		< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
S Reagent Blank #1	< 0.5	< 0.1	< 0.2	< 0.2	< 0.5	< 0.4
#2		< 0.1	< 0.2	< 0.2	< 0.5	< 0.4

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# ANALYTICAL NARRATIVE

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## Element One Analytical Narrative

Client:	Clean Air Engineering	Element One #:	11024
Client ID:	North & South Broward	Analyst:	ESS
Method:	M29	Dates Received:	06/30/08
Analytes:	Hg	Dates Analyzed:	07/10-14/08

### Summary of Analysis

The Method 29 samples were digested, prepared, and analyzed according to Method 29 protocol. Samples were analyzed for mercury on a PerkinElmer FIMS-100 CVAA mercury analyzer.

### Detection Limits

The FIMS-100 CVAA instrument reporting limit for mercury was 0.004 µg per aliquot analyzed.

### Analysis QA/QC

Duplicate analyses relative percent difference (RPD) and spike sample recovery data are summarized in the Quality Control Section. All QA/QC data was within the criteria of the method.

### Additional Comments

The reported results have not been corrected for any blank values or spike recovery values.

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# QUALITY CONTROL SUMMARY

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## Summary of Quality Control Data

### Mercury Duplicate Analysis RPD

(Method 29 QC limits: < %10 for RPD)

Run Number	Front half	H <sub>2</sub> O <sub>2</sub> /HNO <sub>3</sub>	Empty Imp	KMnO <sub>4</sub>	HCl
U1 FF Outlet N R1	NA	0.0%	NA	NA	NA
U1 FF Outlet N R2	NA	0.1%	NA	NA	NA
U1 FF Outlet N R3	NA	2.6%	NA	NA	NA
N Field Blank	NA	NA	NA	NA	NA
N Reagent Blank	NA	NA	NA	NA	NA
U1 FF Outlet S R4	NA	0.0%	NA	NA	NA
U1 FF Outlet S R5	NA	0.2%	NA	NA	NA
U1 FF Outlet S R6	NA	0.0%	NA	NA	NA
S Field Blank	NA	NA	NA	NA	NA
S Reagent Blank	NA	NA	NA	NA	NA

### Mercury Spike Recoveries

(Method 29 QC limits: ±25% for Spike Recoveries)

Run Number		Front half	H <sub>2</sub> O <sub>2</sub> /HNO <sub>4</sub>	Empty Imp	KMnO <sub>4</sub>	HCl
U1 FF Outlet N R3	#1	108%	94%	97%	86%	91%
	#2	106%	94%	98%	86%	90%
U1 FF Outlet S R6	#1	108%	103%	96%	93%	94%
	#2	107%	104%	97%	94%	94%

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# SAMPLE CUSTODY

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CHAIN OF CUSTODY FORM

CLIENT Wheelabrator  
 PLANT North Broward  
 PROJECT MANAGER Scott Brown

PROJECT NO. 10455  
 DEPT. 66

NO. OF CONTAINERS

ORIGINAL VOLUME


ANALYSIS REQUESTED

ADDITIONAL INFORMATION

CLEANAIR

LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX	NO. OF CONTAINERS	ORIGINAL VOLUME	Hg	ADDITIONAL INFORMATION					
	1	Unit 1 FF Outlet	6/23/08	Filter	1	-	x						
	1			Front-Half 0.1N HNO3 Rinse	1	102	x						
	1			Imp. 1,2,3 + 0.1N HNO3 Rinse	1	744	x						
	1			Imp. 4 + 0.1N HNO3 Rinse	1	103	x						
	1			Imp. 5,6 KMnO4+H2O Rinse	1	425	x						
	1			Imp. 5,6 HCl Rinse	1	225	x						
	2		6/23/08	Filter	1	-	x						
	2			Front-Half 0.1N HNO3 Rinse	1	100	x						
	2			Imp. 1,2,3 + 0.1N HNO3 Rinse	1	744	x						
	2			Imp. 4 + 0.1N HNO3 Rinse	1	101	x						
	2			Imp. 5,6 KMnO4+H2O Rinse	1	431	x						
	2	V		Imp. 5,6 HCl Rinse	1	226	x						

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Courier: FEDEX	Date / Time	Relinquished by: (Signature)	Date / Time	Received for Analysis by:	Date / Time

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CHAIN OF CUSTODY FORM

CLIENT Wheelabrator  
 PLANT North Broward  
 PROJECT MANAGER Scott Brown

PROJECT NO. 10455  
 DEPT. 66

NO. OF CONTAINERS

ORIGINAL VOLUME


ANALYSIS REQUESTED

ADDITIONAL INFORMATION

CLEANAIR

LAB NO.	RINSE NO.	TEST LOCATION	DATE	SAMPLE MATRIX	NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED	ADDITIONAL INFORMATION
	3	Unit 1 EE Outlet	6/27/08	Filter	1	100	x	
	3			Front-Half 0.1N HNO3 Rinse	1	100	x	
	3			Imp. 1,2,3 + 0.1N HNO3 Rinse	1	740	x	
	3			Imp. 4 + 0.1N HNO3 Rinse	1	101	x	
	3			Imp. 5,6 KMnO4+H2O Rinse	1	432	x	
	3			Imp. 5,6 HCl Rinse	1	225	x	
	FB		6/27/08	Filter	1	—	x	
	FB			Front-Half 0.1N HNO3 Rinse	1	100	x	
	FB			Imp. 1,2,3 + 0.1N HNO3 Rinse	1	300	x	
	FB			Imp. 4 + 0.1N HNO3 Rinse	1	100	x	
	FB			Imp. 5,6 KMnO4+H2O Rinse	1	447	x	
	FB	V		Imp. 5,6 HCl Rinse	1	225	x	

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CHAIN OF CUSTODY FORM

CLIENT	<u>Wheelabrator</u>	PROJECT NO.	<u>10455</u>
PLANT	<u>North Broward</u>	DEPT.	<u>66</u>
PROJECT MANAGER	<u>Scott Brown</u>		

CLEANAIR				NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED			ADDITIONAL INFORMATION
LAB ID	RUN NO	TEST LOCATION	DATE			SAMPLE MATRIX	A	B	
	4	Unit 1 Filter	6/28/08	1	100	x			
	4			1	100	x			
	4			1	100	x			
	4			1	103	x			
	4			1	103	x			
	4			1	103	x			
	4			1	103	x			
	5	6/28/08 Filter		1	-	x			
	5			1	109	x			
	5			1	102	x			
	5			1	102	x			
	5			1	434	x			
	5	V		1	25	x			

Relinquished by: (Signature) <u>Paul Doak</u>	Date / Time <u>6/28/08 17:00</u>	Received by: (Signature) <u>Eric Doak</u>	Date / Time <u>6/30/08 08:19</u>	Relinquished by: (Signature)	Date / Time
Courier: <u>Fed Ex</u>	Date / Time	Relinquished by: (Signature)	Date / Time	Received for Analysis by:	Date / Time

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CHAIN OF CUSTODY FORM

CLIENT <u>Wheelabrator</u>	PROJECT NO. <u>10455</u>	NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED				ADDITIONAL INFORMATION
PLANT <u>North Broward</u>	DEPT. <u>66</u>							
PROJECT MANAGER <u>Scott Brown</u>								

CLEANING LAB NO.	CONTAINER	ANALYSIS	NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED	ADDITIONAL INFORMATION
	Unit 7 PP Outlet	Filter				
5		Front-Half 0.1N HNO3 Rinse	1	100	x	
6		Imp. 1,2,3 + 0.1N HNO3 Rinse	1	77L	x	
6		Imp. 4 + 0.1N HNO3 Rinse	1	100	x	
6		Imp. 5,6 KMnO4+H2O Rinse	1	447	x	
6	V	Imp. 5,6 HCl Rinse	1	225	x	
		Filter				
		Front-Half 0.1N HNO3 Rinse				
		Imp. 1,2,3 + 0.1N HNO3 Rinse				
		Imp. 4 + 0.1N HNO3 Rinse				
		Imp. 5,6 KMnO4+H2O Rinse				
		Imp. 5,6 HCl Rinse				

Relinquished by: (Signature) <u>Eric Doak</u>	Date / Time <u>6/20/08 1700</u>	Received by: (Signature) <u>Scott Brown</u>	Date / Time <u>6/30/08 0849</u>	Relinquished by: (Signature)	Date / Time
Courier: <u>FED EX</u>	Date / Time	Relinquished by: (Signature)	Date / Time	Received for Analysis by:	Date / Time

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Forwarding Lab: <u>Element One</u> <u>Wilmington, NC</u>	Eric Doak Signature <u>Eric M. Doak</u>	

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CHAIN OF CUSTODY FORM

CLIENT <u>Wheelabrator</u>	PROJECT NO. <u>10455</u>	NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED				ADDITIONAL INFORMATION
PLANT <u>North Broward</u>	DEPT. <u>63</u>							
PROJECT MANAGER <u>Scott Brown</u>								

CLEANAIR		TEST LOCATION	DATE	SAMPLE MATRIX	NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED				ADDITIONAL INFORMATION
LAB NO.	RUN NO.										
	NA	Reagent Blank	<u>6/12/09</u>	3 Quartz Filters	1	NA	x				
	NA	Reagent Blank		0.1N HNO3	1	300	x				
	NA	Reagent Blank		DI H <sub>2</sub> O	1	100	x				
	NA	Reagent Blank		5% HNO <sub>3</sub> / 10% H <sub>2</sub> O <sub>2</sub>	1	<del>300</del>	x				<u>200uL</u>
	NA	Reagent Blank		4% KMnO <sub>4</sub> / 10% H <sub>2</sub> SO <sub>4</sub>	1	<del>400</del>	x				<u>350uL</u>
	NA	Reagent Blank		8 N HCl / DI H <sub>2</sub> O	1	<del>225</del>	x				<u>215uL</u>

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Relinquished by: (signature) <u>Eric Doak</u>	Date/Time <u>6/12/09</u>	Received by: (signature) <u>Scott Brown</u>	Date/Time <u>6/12/09</u>	Relinquished by: (signature) <u>Eric Doak</u>	Date/Time <u>6/12/09</u>	Received by: (signature) <u>Scott Brown</u>	Date/Time <u>6/12/09</u>
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CHAIN OF CUSTODY FORM

CLIENT Wheelabrator PROJECT NO. 10455  
 PLANT South Broward DEPT. 66  
 PROJECT MANAGER Scott Brown

CLEANAIR LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX	NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED				ADDITIONAL INFORMATION	
							PH	TOC	THC	Other		
	1	Unit 1 FF Outlet	12/27/08	Filter	1	1						
	2		25	Front-Half 0.1N HNO3 Rinse	1	707	x					138 ml
	4			Imp. 1,2,3 + 0.1N HNO3 Rinse	1	708	x					706 ml
	4			Imp. 4 + 0.1N HNO3 Rinse	1	700	x					102 ml
	4			Imp. 5,6 KMnO4+H2O Rinse	1	700	x					432 ml
	4			Imp. 5,6 HCl Rinse	1	705	x					215 ml
	5		12/29/08	Filter	1	1	x					110 ml
	5			Front-Half 0.1N HNO3 Rinse	1	1045	x					5108 - 110 ml
	5			Imp. 1,2,3 + 0.1N HNO3 Rinse	1	1063	x					766 ml 742 ml
	5			Imp. 4 + 0.1N HNO3 Rinse	1	100	x					105 ml
	5			Imp. 5,6 KMnO4+H2O Rinse	1	418	x					405 ml 425 ml
	5	V	V	Imp. 5,6 HCl Rinse	1	215	x					215 ml

Relinquished by: (Signature) <i>Eric Doak</i>	Date / Time 12/28/08 1700	Received by: (Signature) <i>Lisa Braton</i>	Date / Time 6/30/08 0849	Relinquished by: (Signature)	Date / Time
Courier: FED EX	Date / Time	Relinquished by: (Signature)	Date / Time	Received for Analysis by:	Date / Time

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CHAIN OF CUSTODY FORM

CLIENT <u>Wheelabrator</u>	PROJECT NO. <u>10455</u>	NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED				ADDITIONAL INFORMATION
PLANT <u>South Broward</u>	DEPT. <u>66</u>							
PROJECT MANAGER <u>Scott Brown</u>								

CLEANAIR LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX	NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED				ADDITIONAL INFORMATION	
	106	Unit 1 FF Outlet	6/29/08	Filter	1	119	x					
	36			Front-Half 0.1N HNO3 Rinse	1	108	x					
	26			Imp. 1,2,3 + 0.1N HNO3 Rinse	1	758	x					
	36			Imp. 4 + 0.1N HNO3 Rinse	1	100	x					
	36			Imp. 5,6 KMnO4+H2O Rinse	1	465	x					
	26			Imp. 5,6 HCl Rinse	1	215	x					
	FB		6/24/08	Filter	1	-	x					
	FB			Front-Half 0.1N HNO3 Rinse	1	100	x					70815
	FB			Imp. 1,2,3 + 0.1N HNO3 Rinse	1	300	x					
	FB			Imp. 4 + 0.1N HNO3 Rinse	1	100	x					
	FB			Imp. 5,6 KMnO4+H2O Rinse	1	420	x					
	FB	V	V	Imp. 5,6 HCl Rinse	1	220	x					

Relinquished by: (Signature) <i>Eric Doak</i>	Date / Time 6/29/08 1700	Received by: (Signature) <i>Lisa Braton</i>	Date / Time 6/30/08 0849	Relinquished by: (Signature)	Date / Time
Courier: FED EX	Date / Time	Relinquished by: (Signature)	Date / Time	Received for Analysis by:	Date / Time

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CHAIN OF CUSTODY FORM


CLIENT Wheelabrator  
 PLANT South Broward  
 PROJECT MANAGER Scott Brown

PROJECT NO. 10455  
 DEPT. 66

NO. OF CONTAINERS  
 ORIGINAL VOLUME  
 ANALYSIS REQUESTED

LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX	NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED				ADDITIONAL INFORMATION	
	(EA) 47	Unit 1 FF Outlet	6/26/08	Filter	1	-	x					
	47			Front-Half 0.1N HNO3 Rinse	1	100	x					
	47			Imp. 1,2,3 + 0.1N HNO3 Rinse	1	779	x					
	47			Imp. 4 + 0.1N HNO3 Rinse	1	101	x					
	47			Imp. 5,6 KMnO4+H2O Rinse	1	424	x					
	47			Imp. 5,6 HCl Rinse	1	225	x					
	(EA) 58		6/26/08	Filter	1	-	x					
	58			Front-Half 0.1N HNO3 Rinse	1	105	x					
	58			Imp. 1,2,3 + 0.1N HNO3 Rinse	1	770	x					
	58			Imp. 4 + 0.1N HNO3 Rinse	1	102	x					
	58			Imp. 5,6 KMnO4+H2O Rinse	1	422	x					
	58	V		Imp. 5,6 HCl Rinse	1	225	x					

Relinquished by: (Signature) <i>Eric Doak</i>	Date / Time 6/28/08 1700	Received by: (Signature) <i>Loa Braton</i>	Date / Time 6/30/08 0849	Relinquished by: (Signature)	Date / Time
Courier: <i>FED EX</i>	Date / Time	Relinquished by: (Signature)	Date / Time	Received for Analysis by:	Date / Time

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CHAIN OF CUSTODY FORM

CLIENT Wheelabrator  
 PLANT South Broward  
 PROJECT MANAGER Scott Brown

PROJECT NO. 10455  
 DEPT. 66

CONTAINER

LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX
	<u>59</u>	<u>Unit 1 FF Outlet</u>	<u>6/26/08</u>	<u>Filter</u>
	<u>89</u>			<u>Front-Half 0.1N HNO3 Rinse</u>
	<u>89</u>			<u>Imp. 1,2,3 + 0.1N HNO3 Rinse</u>
	<u>89</u>			<u>Imp. 4 + 0.1N HNO3 Rinse</u>
	<u>89</u>			<u>Imp. 5,6 KMnO4+H2O Rinse</u>
	<u>89</u>	<u>V</u>		<u>Imp. 5,6 HCl Rinse</u>
				<u>Filter</u>
				<u>Front-Half 0.1N HNO3 Rinse</u>
				<u>Imp. 1,2,3 + 0.1N HNO3 Rinse</u>
				<u>Imp. 4 + 0.1N HNO3 Rinse</u>
				<u>Imp. 5,6 KMnO4+H2O Rinse</u>
				<u>Imp. 5,6 HCl Rinse</u>

NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED				ADDITIONAL INFORMATION
		As Received	As Preserved	As Analyzed	As Reported	
1	100	x				
1	100	x				
1	776	x				
1	100	x				
1	427	x				
1	225	x				

Relinquished by: (Signature) <u>Eric Doak</u>	Date / Time <u>6/26/08 1700</u>	Received by: (Signature) <u>Lisa Draton</u>	Date / Time <u>6/30/08 0849</u>	Relinquished by: (Signature)	Date / Time
Courier:	Date / Time	Relinquished by: (Signature)	Date / Time	Received for Analysis by:	Date / Time

Special Handling Instructions


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Wilmington, NC

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This form was completed by:

Eric Doak  
 Signature

6/26/08  
 Date



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 Palatine, IL 60067

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CHAIN OF CUSTODY FORM


CLIENT Wheelabrator  
 PLANT South Broward  
 PROJECT MANAGER Scott Brown

PROJECT NO. 10455  
 DEPT. 66

NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED				ADDITIONAL INFORMATION
		1	2	3	4	

CLEANAIR LAB NO.	NO. OF CONTAINERS	TEST LOCATION	DATE	SAMPLE MATRIX	NO. OF CONTAINERS	ORIGINAL VOLUME	1	2	3	4	ADDITIONAL INFORMATION
NA	1	Reagent Blank	6/20/08	3 Quartz Filters	1	NA	x				
NA	1	Reagent Blank		0.1N HNO3	1	300	x				
NA	1	Reagent Blank		DI H2O	1	100	x				
NA	1	Reagent Blank		5% HNO3 / 10% H2O2	1	200	x				
NA	1	Reagent Blank		4% KMnO4 / 10% H2SO4	1	100	x				
NA	1	Reagent Blank		8 N HCl / DI H2O	1	225	x				

Relinquished by: (Signature) <i>Eric M. Doak</i>	Date / Time <i>6/20/08 12:00</i>	Received by: (Signature) <i>Scott Brown</i>	Date / Time <i>6/30/08 0849</i>	Relinquished by: (Signature)	Date / Time
Counter: <i>FEA EX</i>	Date / Time	Relinquished by: (Signature)	Date / Time	Received for Analysis by:	Date / Time

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## Analytical Calculations

### Metals-

$$\text{Element Results } (\mu\text{g}) = \text{ICP Results } (\mu\text{g/L}) * \text{Dilution} * \text{Final Volume (L)}$$

### Where-

ICP Results= Raw sample concentration (ppb)--*ICP-Data Sheet*

Dilution=  $\frac{\text{Diluted Volume--ICP-MS Run Sheet}}{\text{Aliquot}}$

Final Volume=FH=Final Volume (FV)--*Sample Submission*

BH= $\frac{\text{Received Volume (BV). * Final Volume (FV)--Sample Submission}}{\text{Aliquot (Used)}}$

Combined Results=FH+BH

### Mercury-

$$\text{Mercury Results } (\mu\text{g}) = \frac{\text{CVAA Results } (\mu\text{g}) * \text{Final Volume (ml)}}{\text{Aliquot (ml)}}$$

### Where-

CVAA Results= Raw sample reading ( $\mu\text{g}$ )--*Hg-Data Sheet*

Aliquot= Sample Aliquot (Alq.)--*Hg-Data Sheet*

Final Volume=Final Volume (FV)\*--*Sample Submission*

\* With the exception of the BH fraction where-  
=Received Volume (BV)--*Sample Submission*

### elementOne

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**BEST AVAILABLE COPY**

One AIR TESTING SAMPLE SUBMISSION FORM Lab ID 11024

Analysis Due Date 07.10.08  
QA/QC/Report Due Date 07.11.08

Client Clean Air  
Project No 10455 - North & South Broward

Date Rec 06.30.08  
Time Rec 0849

HNO<sub>3</sub> Lot: 07-300 Ref. Lot: 5107-13 FCI Lot: 4198010 Ref. Method: 29  
Volume Marked Y/N Volume Loss Y/N

**Sample Identification**

1	U1 FF Outlet North A1	4	North Field Blank	6	U1 FF Outlet North R4
2	U1 FF Outlet North B2	5	North Reagent Blank	7	U1 FF Outlet North R5
	U1 FF Outlet North B2 Duplicate				U1 FF Outlet North R5 Duplicate
3	U1 FF Outlet North R2			8	U1 FF Outlet North R6
	U1 FF Outlet North R2 Spike				U1 FF Outlet North R6 Spike

Analyses Requested: Samples 1-5 Hg  
Samples 6-8 ARCHIVE

Runs / FB	Acetone (FH)		HNO <sub>3</sub> (FH)		5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub> (BH)		HNO <sub>3</sub> (A)		KMnO <sub>4</sub> (B)		HCl (C)		
	BV ml	FV ml	BV ml	FV ml	BV ml	Used	FV ml	BV ml	FV ml	BV ml	FV ml	BV ml	FV ml
1								106	200	390	500	220	400
2.D								104		390		230	
3.S								104		400		230	
4								104		400		230	
6													
7.D													
8.S													

**Reagent Blank**

Lab ID	Prep on	SV, ml	BV, ml	Used	FV, ml	pH	Prep By / Date
5	C-7 FH Acetone Blank						
	C-8 FH 0.1N HNO <sub>3</sub>			100			
	C-8 FH 0.1N HNO <sub>3</sub>		30		306		RLC 7/10/08
	C-8 B H <sub>2</sub> O	115		33			
	C-9 BH 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	350	30	100			
	C-10 B 5% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	230			400		
	C-11 C H <sub>2</sub> O						
	C-12 FH H <sub>2</sub> O						

**Lab Communications**

SS Page1 of 2

SS by Paul Smith  
7/1/2008 5:34:31 PM

FH Prep By/Date ESS 7/1/08 A Prep By/Date RLC 7/10/08  
BH Prep By/Date RLC 7/10/08 B Prep By/Date ESS 7/10/08  
BH/FH Prep By/Date N/A C Prep By/Date ESS 7/10/08  
Labeled By/Date FDS 7/1/08 ID Verification By/Date RLC 7/10/08

11024

One

Method 29 Microwave Worksheet

Lab ID # e

Client: Chen H

Date Digested: 7/10/8 Initials: ESS Worksheet Prepared by: ESS

Auto Sample Loc.	Sample Lab ID	Sample Weight (g)	# of filters digested	Spike	Prep Volume (ml)	Weight In Micro / Weight Out Micro	Units
2	1104-1		1		100		
3	-2		1				
4	-3		1				
5	-4		1				
6	-5		1				
7	-6		1				
8	-7		1				
9	-8		1				
10	-9		1				
11	-10		1				
1	11022 - LRB				40		
12	-11022-1		.2120g				
13	-2		.2050g				
14	-3		.2062g				
15	-3		.2414g				
16	LRB off						

Element One, Inc. Form 104 - Rev. 10/80

6mls H1003 073602  
2mls HF 5107113

114





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WHEELABRATOR NORTH BROWARD, INC.  
POMPANO BEACH, FL

Client Reference No: 14800198  
CleanAir Project No: 10455-6

**PLANT DATA**

H

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**WHEELABRATOR NORTH BROWARD  
TONS OF REFUSE PROCESSED PER STACK TEST RUN LOG**

<b>UNIT #1</b>						
<b>Date</b>	<b>Test</b>	<b>Method #</b>	<b>Run #</b>	<b>Steam (klb/hr)</b>	<b>Run Length (hr)</b>	<b>Trash Processed (tons)</b>
6/27/2008	Mercury	29	1	184.8	2.27	76.3
6/27/2008	Mercury	29	2	183.9	2.23	74.6
6/27/2008	Mercury	29	3	183.9	2.33	77.9

**Wheelabrator  
NORTH BROWARD  
Emission Test Log**

Date: 06/27/08  
Start Time: 9:05  
End Time: 11:21

SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIP WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS
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	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O
Unit 1 29 run 1	523.13	324.65	39.08	34.19	4.89	15.55	309.35	6.64	-9.99
Unit 2	503.24	324.36	33.19	23.94	9.25	18.44	311.72	6.53	-8.94
Unit 3	516.30	324.37	39.73	29.50	10.23	15.29	314.43	6.69	-9.84

H - 4

FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNCR CHEM FLOW	STEAM FLOW
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	KLBs/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBs/hr
Unit 1	191.33	876.00	827.76	70.15	-0.15	274.19	1204.52	7.26	184.80
Unit 2	189.67	892.12	829.80	82.45	-0.25	275.06	1166.69	8.63	184.26
Unit 3	191.89	892.69	830.24	80.83	-0.09	280.82	1153.71	9.95	184.76

**Wheelabrator  
NORTH BROWARD  
Emission Test Log**

Date: 06/27/08  
Start Time: 11:40  
End Time: 13:54

SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS
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	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O
Unit 1 29 run 2	530.64	325.38	42.28	35.38	6.90	13.99	310.34	6.86	-10.39
Unit 2	502.07	325.20	32.46	26.58	5.88	18.21	312.69	6.74	-9.04
Unit 3	518.53	325.28	40.60	33.78	6.82	14.56	315.56	6.81	-10.01

H - 5

FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNGR CHEM FLOW	STEAM FLOW
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	KLBS/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBS/hr
Unit 1	189.01	875.56	820.61	73.58	-0.14	273.33	1200.30	6.75	183.89
Unit 2	188.78	891.34	829.51	81.86	-0.24	274.26	1169.56	11.36	183.46
Unit 3	190.74	891.97	832.93	81.58	-0.09	279.92	1159.29	10.76	183.46

**Wheelabrator  
NORTH BROWARD  
Emission Test Log**

Date: 06/27/08  
Start Time: 14:14  
End Time: 16:34

SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS
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	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O
Unit 1 29 run 3	537.80	325.78	44.64	38.63	6.01	13.43	311.31	7.13	-10.82
Unit 2	510.54	325.28	35.30	27.33	7.97	17.01	312.65	6.55	-9.67
Unit 3	527.45	324.51	43.94	35.12	8.82	13.76	315.76	6.77	-10.21

FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNGR CHEM FLOW	STEAM FLOW
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	KLBs/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBs/hr
Unit 1	188.73	875.83	820.82	75.49	-0.16	273.04	1212.86	4.66	183.86
Unit 2	188.80	891.07	829.62	85.37	-0.25	273.90	1160.51	8.03	183.52
Unit 3	190.71	891.52	828.49	86.17	-0.10	279.60	1160.52	8.71	183.82

**Wheelabrator  
NORTH BROWARD  
Emission Test Log**

Date: 06/28/08  
Start Time: 6:47  
End Time: 9:02

SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS
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	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O
Unit 1 29 run 4	524.24	324.16	38.74	33.32	5.41	15.94	309.86	6.57	-9.83
Unit 2	498.27	325.06	31.05	23.80	7.25	19.69	311.79	6.63	-9.26
Unit 3	481.99	324.56	28.85	23.45	5.39	22.38	312.87	6.00	-8.65

H-7

FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	EGONO OUT TEMP	SH ROLL AVG	SOCR CHEM FLOW	STEAM FLOW
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	KLBS/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBS/hr
Unit 1	190.99	873.21	826.53	66.46	-0.10	269.72	1199.92	3.36	184.61
Unit 2	189.33	889.21	828.37	82.11	-0.10	269.08	1159.41	9.20	184.31
Unit 3	160.63	883.82	820.95	73.68	-0.25	276.45	1052.65	3.84	156.06

**Wheelabrator  
NORTH BROWARD  
Emission Test Log**

Date: 06/28/08  
Start Time: 9:19  
End Time: 11:34

SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS
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	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O
Unit 1 29 run 5	526.17	325.34	39.04	33.58	5.46	15.47	310.02	6.77	-9.96
Unit 2	504.85	325.27	32.86	27.31	5.55	18.38	312.79	6.84	-9.07
Unit 3	510.61	325.32	39.20	31.84	7.36	15.64	314.90	6.73	-10.11

8 - H

FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNCR CHEM FLOW	STEAM FLOW
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	KLBs/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBs/hr
Unit 1	190.06	876.01	824.86	67.68	-0.09	273.72	1199.10	3.34	184.18
Unit 2	189.33	892.20	832.15	83.98	-0.09	272.68	1161.64	8.03	183.60
Unit 3	192.25	893.17	837.93	81.47	-0.25	280.35	1140.82	10.82	184.47

**Wheelabrator  
NORTH BROWARD  
Emission Test Log**

Date: 06/28/08  
Start Time: 11:52  
End Time: 14:05

SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS
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	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O
Unit 1 29 run 6	534.29	324.75	41.75	36.87	4.89	14.19	310.46	6.70	-10.06
Unit 2	506.42	324.87	33.66	24.89	8.77	17.52	312.59	6.77	-8.98
Unit 3	503.23	324.79	35.76	29.72	6.04	17.25	314.33	6.33	-9.40

6 - H

FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNGR CHEM FLOW	STEAM FLOW
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	KLBS/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBS/hr
Unit 1	190.36	875.80	825.27	70.03	-0.09	272.66	1199.43	2.92	184.26
Unit 2	189.74	891.11	829.54	84.10	-0.10	271.28	1161.52	7.51	184.31
Unit 3	184.31	890.32	831.59	77.35	-0.28	279.29	1122.88	9.32	177.06

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WHEELABRATOR NORTH BROWARD, INC.  
POMPANO BEACH, FL

Client Reference No: 14800198  
CleanAir Project No: 10455-6

**PERTINENT CORRESPONDENCE**

I

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**Scott Brown**

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**From:** Faller, Chuck [cfaller@WM.com]  
**Sent:** Monday, June 30, 2008 7:46 AM  
**To:** 'Sbrown (E-mail)'  
**Cc:** Porter, Timothy  
**Subject:** FW: Wheelabrator North & South Broward quarterly mercury testing

Please include this email in the North and South Broward quarterly reports.

-----Original Message-----

**From:** Faller, Chuck  
**Sent:** Wednesday, June 25, 2008 1:24 PM  
**To:** 'william.forrest@dep.state.fl.us'  
**Subject:** Wheelabrator North & South Broward quarterly mercury testing

Second quarter mercury stack testing began yesterday (June 24th) at South Broward. Unfortunately, after the first three runs were completed, Clean Air Engineering notified me that they collected the samples with a broken Peto tube and the three runs had to be discarded. Therefore, we will be sampling the first three runs today (June 25). The second set of three runs will be collected tomorrow (June 26). North Broward testing will now be completed on Friday and Saturday (June 27 and 28).

If you have any questions please give me a call at (954) 581-6606, ext 255.

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