



**Wheelabrator North Broward Inc.**

A Waste Management Company

2600 N.W. 48th Street  
Pompano Beach, FL 33073  
(954) 971-8701  
(954) 971-8703 Fax

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**OCT 24 2005**

**BUREAU OF AIR REGULATION**

October 18, 2005

#70031010000154666145

Mr. Laxmana Tallam, P.E.  
Air Permitting/Compliance/Enforcement Supervisor  
Florida Department of Environmental Protection  
Southeast District  
400 North Congress Ave., Suite 200  
West Palm Beach, FL 33401

Re: Wheelabrator North Broward  
F.A.C. 62-296.416 Quarterly Mercury Stack Testing  
Third Quarter of 2005, Report Submittal

Dear Mr. Tallam:

As required by F.A.C. 62-296.416, please find enclosed the 2005 third quarter report on mercury stack testing which was conducted on Unit #3.

I, the undersigned, am a responsible official, as defined in Rule 62-210.200, F.A.C., of the Title V source addressed in this submittal. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements and information in this document are true, accurate and complete.

If there are any questions, please contact this office at (954) 971-8701.

Sincerely,

Christopher M. Carey  
Regional Vice President

cc: USEPA, Region IV, Pesticides and Toxics Management Division, Air & EPCRA Enforcement  
Branch, Air Enforcement Section #70031010000154666152  
FDEP, Tallahassee, Bureau of Air Regulation, New Source Review Section,  
#70031010000154666169  
Broward County Department of Planning and Environmental Protection, Air Quality Division  
#70031010000154666176

Chuck Faller (with)  
Matt Killeen (without)  
Tim Porter (without)  
Sandy Gutner - MPI - (with)  
Jeff Turpin - BCOIWM (without)  
File: 3.7.2 (without)  
5.1.3.2 (without)

s:admin/receptionist101805





Wheelabrator North Broward  
2600 NW 48<sup>th</sup> Street  
Pompano Beach, FL 33073

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**BUREAU OF AIR REGULATION**

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**REPORT ON MERCURY TESTING**

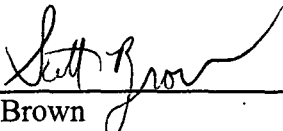
Performed for:  
**WHEELABRATOR NORTH BROWARD**  
**UNIT 3 FF OUTLET**  
**POMPANO BEACH, FLORIDA**

Client Reference No: 14500124  
CleanAir Project No: 9708-4  
Revision 0: October 14, 2005

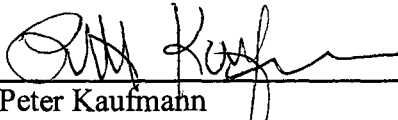
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To the best of our knowledge, the data presented in this report are accurate, complete, error free, legible and representative of the actual emissions during the test program.

Submitted by,

  
\_\_\_\_\_  
Scott Brown  
Project Manager  
847-654-4544

Reviewed by,

  
\_\_\_\_\_  
Peter Kaufmann  
Manager - Palatine Source  
847-654-4560

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**PROJECT OVERVIEW**

1-1

Wheelabrator North Broward, Inc. operates a Refuse to Energy Facility located in Pompano Beach, Florida. The facility's emission levels are regulated by the Florida Department of Environmental Protection. Wheelabrator North Broward, Inc. contracted Clean Air Engineering (CleanAir) to perform a compliance test program at their municipal waste combustor (MWC) facility in Pompano Beach, Florida. Testing was conducted in accordance with 40 CFR 60 Subpart Cb and applicable sections of PSD-FL-112(B) and PA86-22. The sampling was conducted at the Unit 3 Fabric Filter (FF) Outlet on September 20, 2005.

The testing included the determination of the following constituents:

- moisture (H<sub>2</sub>O);
- oxygen (O<sub>2</sub>);
- carbon dioxide (CO<sub>2</sub>);
- total flow (dscfm);
- mercury (Hg).

Coordinating and observing the field portion of the program were:

- C. Faller - Wheelabrator North Broward, Inc.
- D. Dreska - CleanAir

The schedule of activities is shown in Table 1-1. A summary of the results is presented in Table 1-2 on page 1-2.

**Table 1-1:  
Schedule of Activities**

<u>Date (2005)</u>	<u>Start Time</u>	<u>Stop Time</u>	<u>Unit</u>	<u>Location</u>	<u>Pollutant</u>	<u>Method</u>	<u>Run No.</u>
<u>September 20</u>	08:30	11:18	3	FF Outlet	Mercury	EPA 29	1
	12:04	14:17	3	FF Outlet	Mercury	EPA 29	2
	14:35	16:50	3	FF Outlet	Mercury	EPA 29	3



WHEELABRATOR NORTH BROWARD  
POMPANO BEACH, FLORIDA

Client Reference No: 14500124  
CleanAir Project No: 9708-4

**PROJECT OVERVIEW**

1-2

**Table 1-2:  
Summary of Test Results**

<b>Source Constituent (Units)</b>	<b>Sampling Method</b>	<b>Average Emission</b>	<b>Permit Limit<sup>1</sup></b>
<u>Unit 3 FF Outlet</u>			
Mercury ( $\mu\text{g}/\text{dscm}$ @ 7% $\text{O}_2$ )	EPA M29	6.0	70

<sup>1</sup> Limits obtained from 40 Code of Federal Register part 60 Subpart Cb - Emission Guidelines and Compliance Times for Large Municipal Waste Combustors That Are Constructed on or Before September 20, 1994 published in Federal Register as 62 FR 45123 on December 19, 1995 as modified on August 25, 1997, 40 CFR 60.33b (a) (3), Rule 62-296.416 (3) (b) and PSD-FL-112.

The test conditions and results of analysis are presented in Table 2-1 on page 2-1 and the Quality Control and Quality Assurance Results are shown in Table 2-2 on page 2-2.

**RESULTS**

2-1

**Table 2-1:  
Unit 3 FF Outlet - Mercury**

Run No.	1	2	3	Average
Date (2005)	Sep 20	Sep 20	Sep 20	
Start Time (approx.)	08:30	12:04	14:35	
Stop Time (approx.)	11:18	14:17	16:50	
<b>Process Conditions</b>				
R <sub>P</sub> Steam Production Rate - (Klbs/hour)	182	185	184	184
P <sub>1</sub> SDA Outlet Temperature (°F)	315	306	305	309
<b>Gas Conditions</b>				
O <sub>2</sub> Oxygen (dry volume %)	9.4	9.4	9.6	9.5
CO <sub>2</sub> Carbon dioxide (dry volume %)	9.6	9.8	9.4	9.6
T <sub>s</sub> Sample temperature (°F)	303	296	297	299
B <sub>w</sub> Actual water vapor in gas (% by volume)	24.2	25.1	24.9	24.7
<b>Gas Flow Rate</b>				
Q <sub>a</sub> Volumetric flow rate, actual (acfm)	201,689	190,999	181,267	191,318
Q <sub>std</sub> Volumetric flow rate, dry standard (dscfm)	103,248	97,458	102,308	101,005
<b>Sampling Data</b>				
V <sub>std</sub> Volume metered, standard (dscf)	85.919	82.910	81.984	83.604
%I Isokinetic sampling (%)	102.6	104.9	98.8	102.1
<b>Laboratory Data</b>				
m <sub>n-1b</sub> Fraction 1B Prorated (µg)	<0.1000	<0.1000	<0.1000	
m <sub>n-2b</sub> Fraction 2B Prorated (µg)	10.0180	10.9757	12.8701	
m <sub>n-3a</sub> Fraction 3A Prorated (µg)	<0.2000	<0.2000	<0.2000	
m <sub>n-3b</sub> Fraction 3B Prorated (µg)	<0.5000	<0.5000	<0.5000	
m <sub>n-3c</sub> Fraction 3C Prorated (µg)	0.8182	<0.4000	<0.4000	
m <sub>n</sub> Total matter corrected for allowable blanks (µg)	10.8362	10.9757	12.8701	
<b>Mercury Results - Total</b>				
C <sub>std</sub> Concentration (lb/dscf)	2.8E-10	2.9E-10	3.5E-10	3.1E-10
C <sub>sd7</sub> Concentration @7% O <sub>2</sub> (lb/dscf)	3.4E-10	3.5E-10	4.3E-10	3.7E-10
C <sub>sd</sub> Concentration (µg/dscm)	4.5	4.7	5.5	4.9
C <sub>sd7</sub> Concentration @7% O <sub>2</sub> (µg/dscm)	5.4	5.6	6.8	6.0
E <sub>lb/hr</sub> Rate (lb/hr)	1.7E-03	1.7E-03	2.1E-03	1.9E-03
E <sub>Fd</sub> Rate - Fd-based (lb/MMBtu)	4.8E-06	5.1E-06	6.1E-06	5.3E-06

**RESULTS**

2-2

**Table 2-2:  
Quality Assurance and Quality Control**

<b>RPD RESULTS</b>						
Run Number		FH Front Half	BH H <sub>2</sub> O <sub>2</sub> /HNO <sub>4</sub>	A Empty Impinger	B KMnO <sub>4</sub>	C HCl
U3 FF Outlet R1		NA	0.1%	NA	NA	4.3%
U3 FF Outlet R2		NA	0.6%	NA	NA	NA
U3 FF Outlet R3		NA	0.9%	NA	NA	NA
Field Blank		NA	NA	NA	NA	NA
Reagent Blank		NA	NA	NA	NA	NA
<b>Sample Spike and Recovery</b>						
U3 FF Outlet R3	#1	121%	95%	102%	102%	88%
	#2	121%	95%	102%	100%	90%
<b>Blanks</b>						
Field Blank	#1	< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
	#2	< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
Reagent Blank	#1	< 0.1	< 0.3	< 0.2	< 0.4	< 0.4
	#2	< 0.1	< 0.3	< 0.2	< 0.4	< 0.4

WHEELABRATOR NORTH BROWARD  
POMPANO BEACH, FLORIDA

Client Reference No: 14500124  
CleanAir Project No: 9708-4

## DESCRIPTION OF INSTALLATION

3-1

The North Broward Resource Recovery Facility operates three 750 tons per day municipal refuse fired, water wall boiler trains. The trains were manufactured by Babcock and Wilcox to produce electricity for sale to a local utility company. Each boiler is equipped a spray dryer absorber (SDA) for acid gas removal, followed by a fabric filter (FF) baghouse for the control of particulate emissions. Wheelabrator Air Pollution Control, Inc supplies the control equipment. Each fabric filter baghouse is followed by an induced draft fan, which directs the flue gas to a dedicated flue in a common stack.

Figure 3-1 shows a general schematic for the facility. The testing occurred at the Unit 3 FF Outlet as shown in Figure 3-1.

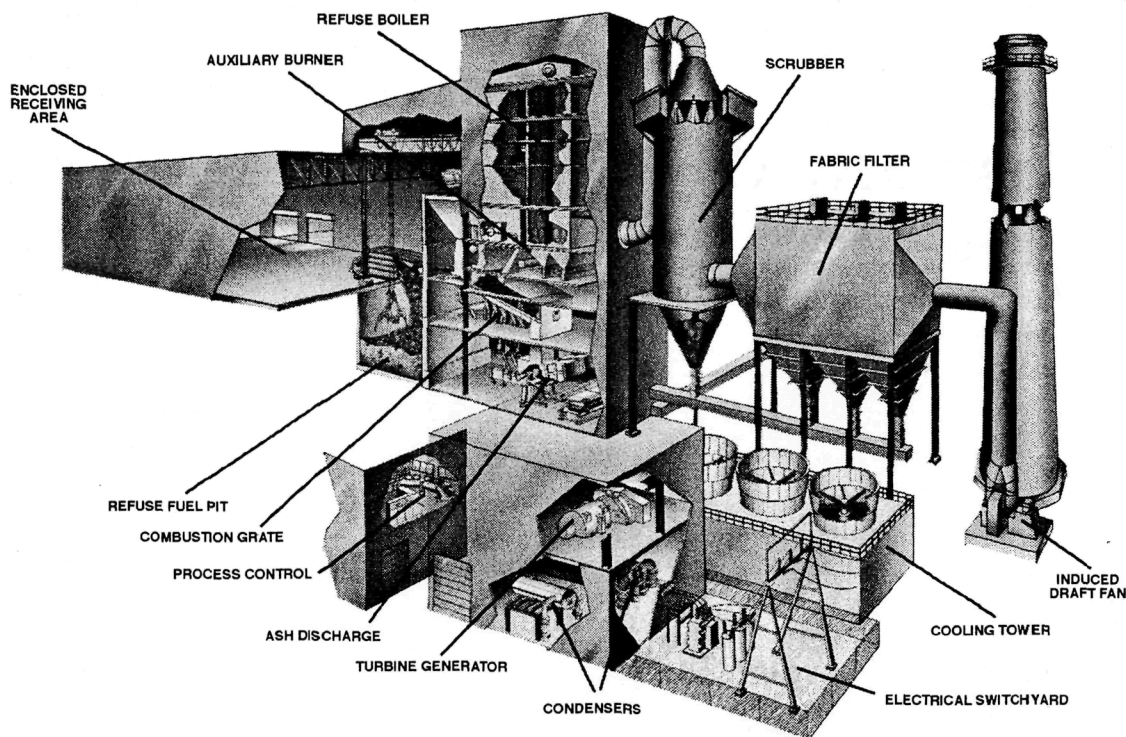


Figure 3-1: General Process Schematic

**Wheelabrator  
NORTH BROWARD  
Emission Test Log**

Date: 20-09-05  
Start Time: 12:04  
End Time: 14:17

SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS
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	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O
Unit 1	517.36	314.49	42.90	37.67	5.23	15.45	292.24	5.90	-10.28
Unit 2	506.73	300.80	43.26	32.65	10.61	15.28	278.36	6.18	-10.14
Unit 3	510.70	305.12	43.28	38.88	4.40	15.32	295.32	5.94	-8.59

G  
-S

FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNCR CHEM FLOW	STEAM FLOW
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	KLBs/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBs/hr
Unit 1	190.46	878.67	831.96	83.05	-0.08	267.96	1177.53	2.53	182.95
Unit 2	189.00	885.47	829.87	80.86	-0.10	269.89	1054.37	9.95	184.39
Unit 3	192.03	888.92	829.54	79.14	-0.10	277.02	1171.53	3.44	184.03

**Wheelabrator  
NORTH BROWARD  
Emission Test Log**

Date: 20-09-05  
Start Time: 14:35  
End Time: 16:50

SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS
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	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O
Unit 1	509.70	307.79	45.89	35.10	10.78	15.28	289.33	5.56	-12.71
Unit 2	503.64	300.02	44.43	29.99	14.44	15.74	274.06	5.92	-10.00
Unit 3	516.81	305.00	46.35	37.76	8.60	15.06	296.42	6.09	-8.50

FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNCR CHEM FLOW	STEAM FLOW
------------------	---------------------	-------------------	-----------------	------------------	-------------------	----------------	-------------------	---------------

	KLBs/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBs/hr
Unit 1	190.81	881.49	832.18	84.54	-0.10	267.17	1165.01	2.83	183.19
Unit 2	188.59	887.29	831.93	82.93	-0.11	269.18	1038.73	9.96	184.03
Unit 3	192.50	891.00	829.89	81.50	-0.10	276.28	1184.09	2.97	184.21

**Wheelabrator  
NORTH BROWARD  
Emission Test Log**

Date: 20-09-05  
Start Time: 08:30  
End Time: 09:45

SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS
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	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O
Unit 1	513.24	309.60	44.33	37.11	7.22	14.75	292.89	4.63	-11.72
Unit 2	511.35	301.94	46.47	32.47	14.00	14.10	286.61	6.27	-10.43
Unit 3	522.68	314.74	47.34	40.36	6.99	13.80	306.76	6.13	-8.02

Q  
1  
3

FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNCR CHEM FLOW	STEAM FLOW
------------------	---------------------	-------------------	-----------------	------------------	-------------------	----------------	-------------------	---------------

	KLBs/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBs/hr
Unit 1	191.32	877.23	835.19	86.38	-0.08	267.74	1134.22	6.09	182.93
Unit 2	189.40	883.28	831.19	87.79	-0.09	269.78	1057.95	9.93	184.20
Unit 3	191.11	886.30	826.19	84.45	-0.08	276.90	1165.99	2.52	182.25

**Wheelabrator  
NORTH BROWARD  
Emission Test Log**

Date: 20-09-05  
Start Time: 10:17  
End Time: 11:18

SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS
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	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O
Unit 1	508.54	309.12	41.73	35.69	6.04	16.24	295.53	6.08	-12.24
Unit 2	506.93	299.40	43.97	33.86	10.11	15.01	281.92	6.24	-10.23
Unit 3	508.19	305.88	43.34	38.16	5.19	15.27	298.19	5.90	-8.52

G - 4

FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNCR CHEM FLOW	STEAM FLOW
------------------	---------------------	-------------------	-----------------	------------------	-------------------	----------------	-------------------	---------------

	KLBS/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBS/hr
Unit 1	188.05	875.87	863.78	82.14	-0.14	267.26	1147.80	2.52	176.73
Unit 2	189.56	882.98	827.58	81.80	-0.09	269.25	1052.66	9.27	185.01
Unit 3	191.46	886.48	825.69	78.83	-0.09	276.40	1158.98	4.21	184.57



WHEELABRATOR NORTH BROWARD  
POMPANO BEACH, FLORIDA

Client Reference No: 14500124  
CleanAir Project No: 9708-4

**OPERATING DATA**

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WHEELABRATOR NORTH BROWARD  
POMPANO BEACH, FLORIDA

Client Reference No: 14500124  
CleanAir Project No: 9708-4

**APPENDIX**

SAMPLE CALCULATIONS .....	A
PARAMETERS .....	B
CALIBRATION DATA .....	C
FIELD DATA .....	D
FIELD DATA PRINTOUTS .....	E
LABORATORY DATA .....	F
OPERATING DATA .....	G

WHEELABRATOR NORTH BROWARD  
POMPANO BEACH, FLORIDA

Client Reference No: 14500124  
CleanAir Project No: 9708-4

**SAMPLE CALCULATIONS**

**A**

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**USEPA Method 29 (Mercury)  
 Sampling, Velocity and Moisture Sample Calculations**

Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

101205 090950

1. Volume of water collected (wscf)

$$V_{wstd} = (0.04707)(V_{lc})$$

Where:

$V_{lc}$	= total volume of liquid collected in impingers and silica gel (ml)	=	581.3	ml
0.04707	= ideal gas conversion factor (ft <sup>3</sup> water vapor/ml or gm)	=	0.04707	ft <sup>3</sup> /ml
$V_{wstd}$	= volume of water vapor collected at standard conditions (ft <sup>3</sup> )	=	27.36	ft <sup>3</sup>

2. Volume of gas metered, standard conditions (dscf)

$$V_{mstd} = \frac{(17.64)(V_m) \left( P_{bar} + \frac{\Delta H}{13.6} \right) (Y_d)}{(460 + T_m)}$$

Where:

$P_{bar}$	= barometric pressure (in. Hg)	=	30.00	in. Hg
$T_m$	= average dry gas meter temperature (°F)	=	92.20	°F
$V_m$	= volume of gas sample through the dry gas meter at meter conditions (dcf)	=	90.46	dcf
$Y_d$	= gas meter correction factor (dimensionless)	=	0.9870	
$\Delta H$	= average pressure drop across meter box orifice (in. H <sub>2</sub> O)	=	1.67	in. H <sub>2</sub> O
17.64	= standard temperature to pressure ratio (°R/in. Hg)	=	17.64	°R/in. Hg
13.6	= conversion factor (in. H <sub>2</sub> O/in. Hg)	=	13.6	in. H <sub>2</sub> O/in. Hg
460	= °F to °R conversion constant	=	460	
$V_{mstd}$	= volume of gas sampled through the dry gas meter at standard conditions (dscf)	=	85.919	dscf

3. Sample gas pressure (in. Hg)

$$P_s = P_{bar} + \left( \frac{P_g}{13.6} \right)$$

Where:

$P_{bar}$	= barometric pressure (in. Hg)	=	30.00	in. Hg
$P_g$	= sample gas static pressure (in. H <sub>2</sub> O)	=	-11.10	in. H <sub>2</sub> O
13.6	= conversion factor (in. H <sub>2</sub> O/in. Hg)	=	13.6	in. H <sub>2</sub> O/in. Hg
$P_s$	= absolute sample gas pressure (in. Hg)	=	29.18	in. Hg

4. Actual water vapor pressure at sample gas temperature less than 212°F (in. Hg)

$$P_v = \frac{e^{\left( \frac{18.3036 - \frac{3816.44}{\frac{5}{9}(T_s - 32) + 273.15 - 46.13}}{25.4} \right)}}{25.4}$$

Where:

$T_s$	= average sample gas temperature (°F)	=	303.04	°F
18.3036	= Antoine coefficient	=	18.3036	°K
3816.44	= Antoine coefficient	=	3816.44	°K
273.15	= temperature conversion factor	=	273.15	°K
46.13	= Antoine coefficient	=	46.13	°K
25.4	= conversion factor	=	25.4	mm Hg/in. Hg
5/9	= Fahrenheit to Celsius conversion factor	=	5/9	°C/°F
32	= temperature conversion (°F)	=	32	°F
$P_v$	= vapor pressure, actual (in. Hg)	=	29.18	in. Hg

5. Water vapor pressure at gas temperature greater than 212°F (in. Hg)

$$P_v = P_s$$

Where:

$P_s$	= absolute sample gas pressure (in. Hg)	=	29.18	in. Hg
$P_v$	= water vapor pressure, actual (in. Hg)	=	29.18	in. Hg

6. Moisture measured in sample (% by volume)

$$B_{wo} = \frac{V_{wstd}}{(V_{mstd} + V_{wstd})}$$

Where:

$V_{mstd}$	= volume of gas sampled through the dry gas meter at standard conditions (dscf)	=	85.919	dscf
$V_{wstd}$	= volume of water collected at standard conditions (scf)	=	27.36	scf
$B_{wo}$	= proportion of water measured in the gas stream by volume	=	0.2415	
		=	24.15	%

7. Saturated moisture content (% by volume)

$$B_{ws} = \frac{P_v}{P_s}$$

Where:

$P_s$	= absolute sample gas pressure (in. Hg)	= 29.18	in. Hg
$P_v$	= water vapor pressure, actual (in. Hg)	= 29.18	in. Hg
$B_{ws}$	= proportion of water vapor in the gas stream by volume at saturated conditions	1.0000	
		= 100.00	%

8. Actual water vapor in gas (% by volume)

$$B_w = \text{MINIMUM } [B_{wo}, B_{ws}]$$

Where:

$B_{ws}$	= proportion of water vapor in the gas stream by volume at saturated conditions	= 1.0000	
$B_{wo}$	= proportion of water measured in the gas stream by volume	= 0.2415	
$B_w$	= actual water vapor in gas	= 0.2415	
		= 24.15	%

9. Nitrogen (plus carbon monoxide) in gas stream (% by volume, dry)

$$N_2 + CO = 100 - CO_2 - O_2$$

Where:

$CO_2$	= proportion of carbon dioxide in the gas stream by volume (%)	= 9.6	%
$O_2$	= proportion of oxygen in the gas stream by volume (%)	= 9.4	%
100	= conversion factor (%)	= 100	%
$N_2+CO$	= proportion of nitrogen and CO in the gas stream by volume (%)	= 81.00	%



10. Molecular weight of dry gas stream (lb/lb-mole)

$$M_d = (M_{CO_2}) \frac{(CO_2)}{(100)} + (M_{O_2}) \frac{(O_2)}{(100)} + (M_{N_2+CO}) \frac{(N_2 + CO)}{(100)}$$

Where:

$M_{CO_2}$	= molecular weight of carbon dioxide (lb/lb-mole)	=	44.00	lb/lb-mole
$M_{O_2}$	= molecular weight of oxygen (lb/lb-mole)	=	32.00	lb/lb-mole
$M_{N_2+CO}$	= molecular weight of nitrogen and carbon monoxide (lb/lb-mole)	=	28.00	lb/lb-mole
$CO_2$	= proportion of carbon dioxide in the gas stream by volume (%)	=	9.6	%
$O_2$	= proportion of oxygen in the gas stream by volume (%)	=	9.4	%
$N_2+CO$	= proportion of nitrogen and CO in the gas stream by volume (%)	=	81.0	%
100	= conversion factor (%)	=	100	%
$M_d$	= dry molecular weight of sample gas (lb/lb-mole)	=	29.91	%

11. Molecular weight of sample gas (lb/lb-mole)

$$M_s = (M_d)(1 - B_w) + (M_{H_2O})(B_w)$$

Where:

$B_w$	= proportion of water vapor in the gas stream by volume	=	0.2415	
$M_d$	= dry molecular weight of sample gas (lb/lb-mole)	=	29.91	lb/lb-mole
$M_{H_2O}$	= molecular weight of water (lb/lb-mole)	=	18.00	lb/lb-mole
$M_s$	= molecular weight of sample gas, wet basis (lb/lb-mole)	=	27.03	lb/lb-mole

12. Velocity of sample gas (ft/sec)

$$V_s = (K_p)(C_p) \left( \sqrt{\Delta P} \right) \left( \sqrt{\frac{(T_s + 460)}{(M_s)(P_s)}} \right)$$

Where:

$K_p$	= velocity pressure constant	=	85.49	
$C_p$	= pitot tube coefficient	=	0.84	
$M_s$	= wet molecular weight of sample gas, wet basis (lb/lb-mole)	=	27.03	lb/lb-mole
$P_s$	= absolute sample gas pressure (in. Hg)	=	29.18	in. Hg
$T_s$	= average sample gas temperature (°F)	=	303.04	°F
$\sqrt{\Delta P}$	= average square roots of velocity heads of sample gas (in. H <sub>2</sub> O)	=	0.744	√in. H <sub>2</sub> O
460	= °F to °R conversion constant	=	460	
$V_s$	= sample gas velocity (ft/sec)	=	52.52	ft/sec

13. Volumetric flow rate of sample gas at actual gas conditions (acfm)

$$Q_a = (60)(A_s)(V_s)$$

Where:

$A_s$	= cross sectional area of sampling location (ft <sup>2</sup> )	=	64.00	ft <sup>2</sup>
$V_s$	= sample gas velocity (ft/sec)	=	52.52	ft/sec
60	conversion factor (sec/min)	=	60	sec/min
$Q_a$	= volumetric flow rate at actual conditions (acfm)	=	201,689	acfm

14. Total flow of sample gas (scfm)

$$Q_s = (Q_a) \left( \frac{P_s}{29.92} \right) \left( \frac{68 + 460}{T_s + 460} \right)$$

Where:

$Q_a$	= volumetric flow rate at actual conditions (acfm)	=	201,689	acfm
$P_s$	= absolute sample gas pressure (in. Hg)	=	29.18	in. Hg
29.92	= standard pressure (in. Hg)	=	29.92	in. Hg
$T_s$	= average sample gas temperature (°F)	=	303.0	°F
68	= standard temperature (°F)	=	68	°F
460	= °F to °R conversion constant	=	460	
$Q_s$	= volumetric flow rate at standard conditions, wet basis (scfm)	=	136,129	scfm

15. Dry flow of sample gas (dscfm)

$$Q_{std} = (Q_s)(1 - B_w)$$

Where:

$B_w$	= proportion of water vapor in the gas stream by volume	=	0.2415	
$Q_s$	= volumetric flow rate at standard conditions, wet basis (scfm)	=	136,129	scfm
$Q_{std}$	= volumetric flow rate at standard conditions, dry basis (dscfm)	=	103,248	dscfm

16. Dry flow of sample gas corrected to 7%O<sub>2</sub> (dscfm)

$$Q_{std7} = (Q_{std}) \left( \frac{20.9 - O_2}{20.9 - 7} \right)$$

Where:

$Q_{std}$	= volumetric flow rate at standard conditions, dry basis (dscfm)	=	103,248	dscfm
$O_2$	= proportion of oxygen in the gas stream by volume (%)	=	9.4	%
20.9	= oxygen content of ambient air (%)	=	20.9	%
7	= oxygen content of corrected gas (%)	=	7.0	%
$Q_{std7}$	= volumetric flow rate at STP and 7%O <sub>2</sub> , dry basis (dscfm)	=	85,421	dscfm

17. Hourly time basis conversion of volumetric flow rate ( $Q_{std}$  example)

$$Q_{std-hr} = (Q_{std-min})(60)$$

Where

$Q_{std-min}$  = volumetric flow rate, english units (ft<sup>3</sup>/min) = 103,248 dscfm

60 = conversion factor (min/hr) = 60 min/hr

$Q_{std-hr}$  = volumetric flow rate, hourly basis (dscf/hr) = 6,194,891 dscf/hr

18. Metric Conversion of Gas Volumes ( $Q_{std}$  example)

$$Q_{std-metric} = (Q_{std-english}) \left( \frac{60}{35.31} \right)$$

Where:

$Q_{std-english}$  = volumetric flow rate, english units (ft<sup>3</sup>/min) = 103,248 dscfm

35.31 = conversion factor (ft<sup>3</sup>/m<sup>3</sup>) = 35.31 ft<sup>3</sup>/m<sup>3</sup>

60 = conversion factor (min/hr) = 60 min/hr

$Q_{std-metric}$  = volumetric flow rate, metric units (m<sup>3</sup>/hr) = 175,443 dry std m<sup>3</sup>/hr

19. Standard to Normal Conversion of Gas Volumes ( $Q_{std}$  example)

$$Q_{Normal} = (Q_{std-metric}) \left( \frac{32 + 460}{68 + 460} \right)$$

Where:

$Q_{std-metric}$  = volumetric flow rate, metric units (dry std m<sup>3</sup>/hr) = 175,443 dry std m<sup>3</sup>/hr

32 = normal temperature (°F) = 32 °F

68 = standard temperature (°F) = 68 °F

460 = standard temperature in Rankine (68°F) = 460

$Q_{Normal}$  = volumetric flow rate, metric units (dry Nm<sup>3</sup>/hr) = 163,481 dry Nm<sup>3</sup>/hr

20. Percent isokinetic (%)

$$I = \frac{(0.09450)(T_s + 460)(V_{mstd})}{(P_s)(V_s)\left(\frac{D_n^2(x)}{(1.44)(4)}\right)(\Theta)(1 - B_w)}$$

Where:

$D_n$	= diameter of nozzle (in)	=	0.276	in.
$B_w$	= proportion of water vapor in the gas stream by volume	=	0.2415	
$P_s$	= absolute sample gas pressure (in. Hg)	=	29.18	in. Hg
$T_s$	= average sample gas temperature (°F)	=	303.0	°F
$V_{mstd}$	= volume of gas sample through the dry gas meter at standard conditions (dscf)	=	85.919	dscf
$V_s$	= sample gas velocity (ft/sec)	=	52.52	ft/sec
$\theta$	= total sampling time (min)	=	125	min
0.0945	= conversion constant	=	0.0945	
460	= °F to °R conversion constant	=	460	
$I$	= percent of isokinetic sampling (%)	=	102.61	%

21. Alternative Method 5 Post-Test Meter Calibration Factor

$$Y_{qa} = \frac{\Theta}{V_m} \sqrt{\frac{(0.0319)(T_m + 460)(28.96)}{(\Delta H_{\oplus})(P_{bar} + \frac{\Delta H}{13.6})(M_d)}} (\sqrt{\Delta H})_{avg}$$

Where:

$\theta$	= total sampling time (min)	=	125	min
$V_m$	= volume of gas sample through the dry gas meter at meter conditions (dcf)	=	90.46	dcf
$T_m$	= average dry gas meter temperature (°F)	=	92.20	°F
$\Delta H_{\oplus}$	= dry gas meter orifice coefficient	=	1.7991	
$P_{bar}$	= barometric pressure (in. Hg)	=	30.00	in. Hg
$\Delta H$	= average pressure drop across meter box orifice (in. H <sub>2</sub> O)	=	1.674	in. H <sub>2</sub> O
$M_d$	= dry molecular weight of sample gas (lb/lb-mole)	=	29.91	lb/lb-mole
$\sqrt{\Delta H}_{avg}$	= average of square root of pressure drop across meter orifice	=	1.286	$\sqrt{\text{in. H}_2\text{O}}$
0.0319	= conversion constant	=	0.0319	
28.96	= molecular weight of ambient air (lb/lb-mole)	=	28.96	lb/lb-mole
13.6	= conversion factor (in. H <sub>2</sub> O/in. Hg)	=	13.6	in. H <sub>2</sub> O/in. Hg
460	= °F to °R conversion constant	=	460	
$Y_{qa}$	= alternative Method 5 post-test meter calibration factor	=	0.9969	

## LOGIC FOR TREATING DETECTION LIMITS (mercury only)

### 1. Logic for Determining Total Blank ( $m_{Total-B}$ ) from 5 Fractions

	CASE 1	CASE 2	CASE 3
	All 5 fractions are D.	1 to 4 fractions are ND	All 5 fractions are ND
<b>Rule</b>			
$ND = 0$	$m_{Total-B} = \text{Sum D, 1-5}$	$m_{Total-B} = \text{Sum D}$	$m_{Total-B} = < \text{Sum ND}$
$ND = 1x$	$m_{Total-B} = \text{Sum D, 1-5}$	$m_{Total-B} = \text{Sum D}$	$m_{Total-B} = < \text{Sum ND}$
$ND = 0.5x$	$m_{Total-B} = \text{Sum D, 1-5}$	$m_{Total-B} = \text{Sum D}$	$m_{Total-B} = < 0.5 \text{ Sum ND}$

### 2. Logic for Determining Total Sample ( $m_{Total-S}$ ) from 5 Fractions

	CASE 1	CASE 2	CASE 3
	All 5 fractions are D.	1 to 4 fractions are ND	All 5 fractions are ND
<b>Rule</b>			
$ND = 0$	$m_{Total-S} = \text{Sum D, 1-5}$	$m_{Total-S} = \text{Sum D}$	$m_{Total-S} = < \text{Sum ND}$
$ND = 1x$	$m_{Total-S} = \text{Sum D, 1-5}$	$m_{Total-S} = < \{\text{Sum D} + \text{Sum ND}\}$	$m_{Total-S} = < \text{Sum ND}$
$ND = 0.5x$	$m_{Total-S} = \text{Sum D, 1-5}$	$m_{Total-S} = < \{\text{Sum D} + 0.5 \text{ Sum ND}\}$	$m_{Total-S} = < 0.5 \text{ Sum ND}$

### 3. Logic for Determining Maximum Allowable Blank Correction ( $m_{T-B-allow}$ )

	CASE 1	CASE 2	CASE 3	CASE 4
	All 5 fractions are D. $m_{Total-B} = D$	1 to 4 sample fractions are ND $m_{Total-B} = D$	All 5 fractions are ND $m_{Total-B} = D$	Any type of fractions $m_{Total-B} = ND$
<b>Rule</b>				
$ND = 0$	$m_{T-B-allow} = M29 \text{ Rule}$	$m_{T-B-allow} = M29 \text{ Rule}^*$	$m_{T-B-allow} = 0$	$m_{T-B-allow} = 0$
$ND = 1x$	$m_{T-B-allow} = M29 \text{ Rule}$	$m_{T-B-allow} = M29 \text{ Rule}^*$	$m_{T-B-allow} = 0$	$m_{T-B-allow} = 0$
$ND = 0.5x$	$m_{T-B-allow} = M29 \text{ Rule}$	$m_{T-B-allow} = M29 \text{ Rule}^*$	$m_{T-B-allow} = 0$	$m_{T-B-allow} = 0$

\* M29 rule using only detected sample quantities for logical comparisons.

### 4. Logic for Determining Blank-Corrected Sample Amount ( $m_n$ )

	CASE 1	CASE 2	CASE 3	CASE 4
	All 5 fractions are D. $m_{Total-S} - m_{T-B-allow} \geq \text{MIN(MDL)}$	1 to 4 sample fractions are ND $m_{Total-S} - m_{T-B-allow} \geq \text{MIN(MDL)}$	All 5 fractions are ND $m_{Total-S}$ and $m_{T-B-allow}$ anything	Any type of fractions $m_{Total-S} - m_{T-B-allow} < \text{MIN(MDL)}$
<b>Rule</b>				
$ND = 0$	$m_n = m_{Total-S} - m_{T-B-allow}$	$m_n = m_{Total-S} - m_{T-B-allow}$	$m_n = < m_{Total-S}$	$m_n = < \text{MIN(MDL)}$
$ND = 1x$	$m_n = m_{Total-S} - m_{T-B-allow}$	$m_n = < [m_{Total-S} - m_{T-B-allow}]$	$m_n = < m_{Total-S}$	$m_n = < \text{MIN(MDL)}$
$ND = 0.5x$	$m_n = m_{Total-S} - m_{T-B-allow}$	$m_n = < [m_{Total-S} - m_{T-B-allow}]$	$m_n = < m_{Total-S}$	$m_n = < \text{MIN(MDL)}$

#### Definitions and Notes

The term "Rule" refers to the rule being implemented for handling non-detectable quantities in summations.

MDL = minimum detection limit.

D = Detectable quantity reported as D.

ND = Non-Detectable quantity reported at a value of ND.

MIN(MDL) = lowest quantity of all detection limits for 5 fractions.

EPA Method 29 Sample Calculations - Mercury Analytical Result

Sample data taken from Run 1

The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

Note: Please see the preceding page concerning treatment of minimum detection limits and mathematical operations on values that are below minimum detection limits.

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1. Total blank amount (µg)

$$m_{total-B} = \sum_{i=1}^n m_{i-B}$$

Where:

$m_{1b-B}$	= mercury amount in blank for Fraction 1b	=	<0.1000	µg
$m_{2b-B}$	= mercury amount in blank for Fraction 2b	=	<0.3000	µg
$m_{3a-B}$	= mercury amount in blank for Fraction 3a	=	<0.2000	µg
$m_{3b-B}$	= mercury amount in blank for Fraction 3b	=	<0.4000	µg
$m_{3c-B}$	= mercury amount in blank for Fraction 3c	=	<0.4000	µg
$m_{total-B}$	= total amount of mercury in blank	=	<1.4000	µg

2. Total sample amount (µg)

$$m_{total-S} = \sum_{i=1}^n m_{i-S}$$

Where:

$m_{1b-S}$	= mercury amount in sample for Fraction 1b	=	<0.1000	µg
$m_{2b-S}$	= mercury amount in sample for Fraction 2b	=	10.0180	µg
$m_{3a-S}$	= mercury amount in sample for Fraction 3a	=	<0.2000	µg
$m_{3b-S}$	= mercury amount in sample for Fraction 3b	=	<0.5000	µg
$m_{3c-S}$	= mercury amount in sample for Fraction 3c	=	0.8182	µg
$m_{total-S}$	= total amount of mercury in sample	=	10.8362	µg

3. Allowable blank correction (µg)

$$m_{T-B-allow} = m_{total-B} \text{ if } m_{total-B} \leq 0.6$$

$$m_{T-B-allow} = \text{MAX} [0.6, \text{MIN} (m_{total-B}, 0.05 \times m_{total-S})] \text{ if } m_{total-B} > 0.6$$

Where:

$m_{total-B}$	= total amount of mercury in blank	=	<1.4000	µg
$m_{total-S}$	= total amount of mercury in sample	=	10.8362	µg
$0.05 \times m_{total-S}$	= 5% of $m_{total-S}$	=	0.5418	µg
MAX	= Arithmetic operator that returns the maximum of two values			
MIN	= Arithmetic operator that returns the minimum of two values			
$m_{T-B-allow}$	= total allowable blank correction	=	0.0000	µg

NOTE: In this case, the second criteria applies.

4. Sample corrected for allowable blank - Total (µg)

$$m_n = m_{total-S} - m_{T-B-allow}$$

Where:

$m_{total-S}$	= total amount of mercury in sample	=	10.8362	µg
$m_{T-B-allow}$	= total allowable blank correction	=	0.0000	µg
$m_n$	= total mercury in sample corrected for allowable blank	=	10.8362	µg

5. Sample corrected for allowable blank - Prorated for each fraction (µg)

$$m_{n-i} = \left( \frac{m_{i-S}}{m_{total-S}} \right) (m_n)$$

Where:

$m_n$	= total mercury in sample corrected for allowable blank	=	10.8362	µg
$m_{1b-S}$	= mercury amount in sample for Fraction 1b	=	<0.1000	µg
$m_{2b-S}$	= mercury amount in sample for Fraction 2b	=	10.0180	µg
$m_{3a-S}$	= mercury amount in sample for Fraction 3a	=	<0.2000	µg
$m_{3b-S}$	= mercury amount in sample for Fraction 3b	=	<0.5000	µg
$m_{3c-S}$	= mercury amount in sample for Fraction 3c	=	0.8182	µg
$m_{total-S}$	= total amount of mercury in sample	=	10.8362	µg
$m_{n-1b}$	= mercury corrected for blank - prorated for Fraction 1b	=	<0.1000	µg
$m_{n-2b}$	= mercury corrected for blank - prorated for Fraction 2b	=	10.0180	µg
$m_{n-3a}$	= mercury corrected for blank - prorated for Fraction 3a	=	<0.2000	µg
$m_{n-3b}$	= mercury corrected for blank - prorated for Fraction 3b	=	<0.5000	µg
$m_{n-3c}$	= mercury corrected for blank - prorated for Fraction 3c	=	0.8182	µg

EPA Method 29 Sample Calculations - Mercury Emissions Results

Sample data taken from Run 1

The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

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1. Mercury concentration (lb/dscf)

$$C_{sd} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{2.205 \times 10^{-3}}{10^6} \right)$$

Where:

$m_n$	= Mercury collected in sample (total $\mu\text{g}$ )	=	10.8362	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	=	85.9190	dscf
$2.205 \times 10^{-3}$	= conversion factor (lb/g)	=	2.205E-03	lb/g
$10^6$	= conversion factor ( $\mu\text{g/g}$ )	=	1.0E+06	$\mu\text{g/g}$
$C_{sd}$	= Mercury concentration (lb/dscf)	=	2.7810E-10	lb/dscf

2. Mercury concentration ( $\mu\text{g/dscm}$ )

$$C_{sd} = \left( \frac{m_n}{V_{mstd}} \right) (35.31)$$

Where:

$m_n$	= Mercury collected in sample (total $\mu\text{g}$ )	=	10.8362	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	=	85.9190	dscf
35.31	= conversion factor (dscf/dscm)	=	35.31	dscf/dscm
$C_{sd}$	= Mercury concentration ( $\mu\text{g/dscm}$ )	=	4.4533E+00	$\mu\text{g/dscm}$

3. Mercury concentration (mg/dscm)

$$C_{sd} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{35.31}{1000} \right)$$

Where:

$m_n$	= Mercury collected in sample (total $\mu\text{g}$ )	=	10.8362	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	=	85.9190	dscf
35.31	= conversion factor (dscf/dscm)	=	35.31	dscf/dscm
1000	= conversion factor ( $\mu\text{g/mg}$ )	=	1000	$\mu\text{g/mg}$
$C_{sd}$	= Mercury concentration (mg/dscm)	=	4.4533E-03	mg/dscm



4. Mercury concentration ( $\mu\text{g}/\text{Nm}^3$  dry)

$$C_{sd} = \left( \frac{m_n}{V_{mstd}} \right) (35.31) \left( \frac{68 + 460}{32 + 460} \right)$$

Where:

$m_n$	= Mercury collected in sample (total $\mu\text{g}$ )	=	10.8362	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	=	85.9190	dscf
35.31	= conversion factor (dscf/dscm)	=	35.31	dscf/dscm
68	= standard temperature ( $^{\circ}\text{F}$ )	=	68	$^{\circ}\text{F}$
32	= normal temperature ( $^{\circ}\text{F}$ )	=	32	$^{\circ}\text{F}$
460	= $^{\circ}\text{F}$ to $^{\circ}\text{R}$ conversion constant	=	460	
$C_{sd}$	= Mercury concentration ( $\mu\text{g}/\text{Nm}^3$ dry)	=	4.7792E+00	$\mu\text{g}/\text{Nm}^3$ dry

5. Mercury concentration corrected to x% oxygen (lb/dscf example)

$$C_{sdx} = C_{sd} \left( \frac{20.9 - x}{20.9 - O_2} \right)$$

Where:

$C_{sd}$	= Mercury concentration (lb/dscf)	=	2.7810E-10	lb/dscf
x	= oxygen content of corrected gas (%)	=	7.0	%
$O_2$	= proportion of oxygen in the gas stream by volume (%)	=	9.4	%
20.9	= oxygen content of ambient air (%)	=	20.9	%
$C_{sdx}$	= Mercury concentration corrected to x% oxygen (lb/dscf)	=	3.3614E-10	lb/dscf @ x% $O_2$

6. Mercury concentration corrected to y% carbon dioxide (lb/dscf example)

$$C_{sdy} = C_{sd} \left( \frac{y}{CO_2} \right)$$

Where:

$C_{sd}$	= Mercury concentration (lb/dscf)	=	2.7810E-10	lb/dscf
y	= carbon dioxide content of corrected gas (%)	=	12.0	%
$CO_2$	= proportion of carbon dioxide in the gas stream by volume (%)	=	9.6	%
$C_{sdy}$	= Mercury conc. corrected to y% carbon dioxide (lb/dscf)	=	3.4762E-10	lb/dscf @ y% $CO_2$

7. Mercury concentration at actual gas conditions (lb/acf example)

$$C_a = C_{sd} \left( \frac{Q_{std}}{Q_a} \right)$$

Where:

$C_{sd}$	= Mercury concentration (lb/dscf)	=	2.7810E-10	lb/dscf
$Q_{std}$	= volumetric flow rate at standard conditions, dry basis (dscfm)	=	103,248	dscfm
$Q_a$	= volumetric flow rate at actual conditions (acfm)	=	201,689	acfm
$C_a$	= Mercury concentration at actual gas conditions (lb/acf)	=	1.4236E-10	lb/acf

8. Mercury emission rate (lb/hr)

$$E_{lb/hr} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{2.205 \times 10^{-3}}{10^6} \right) (Q_{std}) (60)$$

Where:

$m_n$	= Mercury collected in sample (total $\mu\text{g}$ )	=	10.8362	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	=	85.9190	dscf
$2.205 \times 10^{-3}$	= conversion factor (lb/g)	=	2.205E-03	lb/g
$10^6$	= conversion factor ( $\mu\text{g/g}$ )	=	1.0E+06	$\mu\text{g/g}$
$Q_{std}$	= volumetric flow rate at standard conditions, dry basis (dscfm)	=	103,248	dscfm
60	= conversion factor (min/hr)	=	60	min/hr
$E_{lb/hr}$	= Mercury emission rate (lb/hr)	=	1.7228E-03	lb/hr

9. Mercury emission rate (g/s)

$$E_{g/s} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{Q_{std}}{(10^6)(60)} \right)$$

Where:

$m_n$	= Mercury collected in sample (total $\mu\text{g}$ )	=	10.8362	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	=	85.9190	dscf
$Q_{std}$	= volumetric flow rate at standard conditions, dry basis (dscfm)	=	103,248	dscfm
$10^6$	= conversion factor ( $\mu\text{g/g}$ )	=	1.0E+06	$\mu\text{g/g}$
60	= conversion factor (sec/min)	=	60	sec/min
$E_{g/s}$	= Mercury emission rate (g/s)	=	2.1703E-04	g/s

10. Mercury emission rate (Ton/yr)

$$E_{T/yr} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{2.205 \times 10^{-3}}{10^6} \right) (Q_{std}) (60) \left( \frac{Cap}{2000} \right)$$

Where:

$m_n$	= Mercury collected in sample (total $\mu\text{g}$ )	=	10.8362	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	=	85.9190	dscf
$2.205 \times 10^{-3}$	= conversion factor (lb/g)	=	2.205E-03	lb/g
$10^6$	= conversion factor ( $\mu\text{g/g}$ )	=	1.0E+06	$\mu\text{g/g}$
$Q_{std}$	= volumetric flow rate at standard conditions, dry basis (dscfm)	=	103,248	dscfm
60	= conversion factor (min/hr)	=	60	min/hr
Cap	= capacity factor for process (hours operated/year)	=	8,760	hours/yr
2000	= conversion factor (lb/Ton)	=	2000	lb/Ton
$E_{T/yr}$	= Mercury emission rate (Ton/yr)	=	7.5458E-03	Ton/yr

11. Mercury emission rate - Fd-based (lb/MMBtu)

$$E_{Fd} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{2.205 \times 10^{-3}}{10^6} \right) (F_d) \left( \frac{20.9}{20.9 - O_2} \right)$$

Where:

$m_n$	= Mercury collected in sample (total $\mu\text{g}$ )	=	10.8362	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	=	85.9190	dscf
$2.205 \times 10^{-3}$	= conversion factor (lb/g)	=	2.205E-03	lb/g
$10^6$	= conversion factor ( $\mu\text{g/g}$ )	=	1.0E+06	$\mu\text{g/g}$
$F_d$	= ratio of gas volume to heat content of fuel (dscf/MMBtu)	=	9,570	dscf/MMBtu
$O_2$	= proportion of oxygen in the gas stream by volume (%)	=	9.4	%
20.9	= oxygen content of ambient air (%)	=	20.9	%
$E_{Fd}$	= Mercury emission rate - Fd-based (lb/MMBtu)	=	4.8368E-06	lb/MMBtu

12. Mercury emission rate - Fc-based (lb/MMBtu)

$$E_{Fc} = \left( \frac{m_n}{V_{mstd}} \right) \left( \frac{2.205 \times 10^{-3}}{10^6} \right) (F_c) \left( \frac{100}{CO_2} \right)$$

Where:

$m_n$	= Mercury collected in sample (total $\mu\text{g}$ )	=	10.8362	$\mu\text{g}$
$V_{mstd}$	= volume metered, standard (dscf)	=	85.9190	dscf
$2.205 \times 10^{-3}$	= conversion factor (lb/g)	=	2.205E-03	lb/g
$10^6$	= conversion factor ( $\mu\text{g/g}$ )	=	1.0E+06	$\mu\text{g/g}$
$F_c$	= ratio of gas volume to heat content of fuel (dscf/MMBtu)	=	1,820	dscf/MMBtu
$CO_2$	= proportion of oxygen in the gas stream by volume (%)	=	9.6	%
100	= conversion factor	=	100	
$E_{Fc}$	= Mercury emission rate - Fc-based (lb/MMBtu)	=	5.2723E-06	lb/MMBtu

WHEELABRATOR NORTH BROWARD  
POMPANO BEACH, FLORIDA

Client Reference No: 14500124  
CleanAir Project No: 9708-4

**PARAMETERS**

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Wheelabrator North Broward, Inc  
 Clean Air Project No: 9708  
 Unit 3 FF Outlet

**USEPA Method 29 (Mercury)  
 Sampling, Velocity and Moisture Parameters**

Run No.		1	2	3	Average
Date (2005)		Sep 20	Sep 20	Sep 20	
Start Time (approx.)		08:30	12:04	14:35	
Stop Time (approx.)		11:18	14:17	16:50	
<b>Sampling Conditions</b>					
$Y_d$	Dry gas meter correction factor	0.9870	0.9870	0.9870	
$C_p$	Pitot tube coefficient	0.84	0.84	0.84	
$P_g$	Static pressure (in. H <sub>2</sub> O)	-11.1000	-11.0000	30.0000	
$A_s$	Sample location area (ft <sup>2</sup> )	64.0000	64.0000	64.0000	
$P_{bar}$	Barometric pressure (in. Hg)	30.00	30.00	30.00	30.0000
$D_n$	Nozzle diameter (in.)	0.2760	0.2760	0.2760	
$O_2$	Oxygen (dry volume %)	9.4000	9.4000	9.6000	9.4667
$CO_2$	Carbon dioxide (dry volume %)	9.6000	9.8000	9.4000	9.6000
$N_2+CO$	Nitrogen plus carbon monoxide (dry volume %)	81.0000	80.8000	81.0000	80.9333
$V_c$	Total Liquid collected (ml)	581.30	589.30	576.50	
$V_m$	Volume metered, meter conditions (ft <sup>3</sup> )	90.4630	86.6250	86.4300	
$T_m$	Dry gas meter temperature (°F)	92.2000	87.7400	92.6800	
$T_s$	Sample temperature (°F)	303.0400	296.4800	296.5600	298.6933
$\Delta H$	Meter box orifice pressure drop (in. H <sub>2</sub> O)	1.6736	1.5080	1.5080	
$\theta$	Total sampling time (min)	125.0	125.0	125.0	
<b>Flow Results</b>					
$V_{wstd}$	Volume of water collected (ft <sup>3</sup> )	27.3618	27.7384	27.1359	27.4120
$V_{mstd}$	Volume metered, standard (dscf)	85.9190	82.9102	81.9842	83.6045
$P_s$	Sample gas pressure, absolute (in. Hg)	29.1838	29.1912	32.2059	30.1936
$P_v$	Vapor pressure, actual (in. Hg)	29.1838	29.1912	32.2059	30.1936
$B_{wo}$	Moisture measured in sample (% by volume)	24.1539	25.0689	24.8679	24.6969
$B_{ws}$	Saturated moisture content (% by volume)	100.0000	100.0000	100.0000	100.0000
$B_w$	Actual water vapor in gas (% by volume)	24.1539	25.0689	24.8679	24.6969
$\sqrt{\Delta P}$	Velocity head ( $\sqrt{in. H_2O}$ )	0.7437	0.7063	0.7038	0.7180
$M_d$	MW of sample gas, dry (lb/lb-mole)	29.9120	29.9440	29.8880	29.9147
$M_w$	MW of sample gas, wet (lb/lb-mole)	27.0348	26.9498	26.9317	26.9721
$V_s$	Velocity of sample (ft/sec)	52.5232	49.7393	47.2051	49.8225
%I	Isokinetic sampling (%)	102.6093	104.8983	98.8098	102.1058
$Q_a$	Volumetric flow rate, actual (acfm)	201,689	190,999	181,267	191,318
$Q_s$	Volumetric flow rate, standard (scfm)	136,129	130,064	136,171	134,121
$Q_{std}$	Volumetric flow rate, dry standard (dscfm)	103,248	97,458	102,308	101,005
$Q_{std7}$	Volumetric flow rate, dry std @ 7%O <sub>2</sub> (dscfm)	85,421	80,631	83,171	83,074
$Q_a$	Volumetric flow rate, actual (acf/hr)	12,101,341	11,459,925	10,876,049	11,479,105
$Q_s$	Volumetric flow rate, standard (scf/hr)	8,167,718	7,803,838	8,170,250	8,047,269
$Q_{std}$	Volumetric flow rate, dry standard (dscf/hr)	6,194,891	5,847,504	6,138,480	6,060,292
$Q_a$	Volumetric flow rate, actual (m <sup>3</sup> /hr)	342,717	324,552	308,016	325,095
$Q_s$	Volumetric flow rate, standard (m <sup>3</sup> /hr)	231,315	221,009	231,386	227,903
$Q_{std}$	Volumetric flow rate, dry standard (dry m <sup>3</sup> /hr)	175,443	165,605	173,845	171,631
$Q_{std7}$	Volumetric flow rate, dry std @ 7%O <sub>2</sub> (dry m <sup>3</sup> /hr)	145,151	137,011	141,328	141,163
$Q_n$	Volumetric flow rate, normal (Nm <sup>3</sup> /hr)	215,543	205,940	215,610	212,365
$Q_{std}$	Volumetric flow rate, dry normal (Nm <sup>3</sup> /hr)	163,481	154,314	161,992	159,929
$Q_{std7}$	Volumetric flow rate, dry normal @ 7%O <sub>2</sub> (Nm <sup>3</sup> /hr)	135,254	127,669	131,692	131,538

**Comments:**

Average includes 3 runs.

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Wheelabrator North Broward, Inc  
 Clean Air Project No: 9708  
 Unit 3 FF Outlet

**USEPA Method 29  
 Mercury (Hg) Emission Parameters**

Run No.	1	2	3	Average	
Date (2005)	Sep 20	Sep 20	Sep 20		
Start Time (approx.)	08:30	12:04	14:35		
Stop Time (approx.)	11:18	14:17	16:50		
<b>Process Conditions</b>					
R <sub>p</sub>	Steam Production Rate - (Klbs/hour)	182	185	184	184
P <sub>1</sub>	SDA Outlet Temperature (°F)	315	306	305	309
F <sub>d</sub>	Oxygen-based F-factor (dscf/MMBtu)	9,570	9,570	9,570	9,570
F <sub>c</sub>	Carbon dioxide-based F-factor (dscf/MMBtu)	1,820	1,820	1,820	1,820
Cap	Capacity factor (hours/year)	8,760	8,760	8,760	8,760
<b>Gas Conditions</b>					
O <sub>2</sub>	Oxygen (dry volume %)	9.4000	9.4000	9.6000	9.4667
CO <sub>2</sub>	Carbon dioxide (dry volume %)	9.6000	9.8000	9.4000	9.6000
T <sub>s</sub>	Sample temperature (°F)	303.0400	296.4800	296.5600	298.6933
B <sub>w</sub>	Actual water vapor in gas (% by volume)	24.1539	25.0689	24.8679	24.6969
<b>Gas Flow Rate</b>					
Q <sub>a</sub>	Volumetric flow rate, actual (acfm)	201,689	190,999	181,267	181,318
Q <sub>s</sub>	Volumetric flow rate, standard (scfm)	136,129	130,064	136,171	134,121
Q <sub>std</sub>	Volumetric flow rate, dry standard (dscfm)	103,248	97,458	102,308	101,005
Q <sub>std7</sub>	Volumetric flow rate, dry std @ 7% O <sub>2</sub> (dscfm)	85,421	80,631	83,171	83,074
Q <sub>a</sub>	Volumetric flow rate, actual (acf/hr)	12,101,341	11,459,925	10,876,049	11,479,105
Q <sub>s</sub>	Volumetric flow rate, standard (scf/hr)	8,167,718	7,803,838	8,170,250	8,047,269
Q <sub>std</sub>	Volumetric flow rate, dry standard (dscf/hr)	6,194,891	5,847,504	6,138,480	6,060,292
Q <sub>a</sub>	Volumetric flow rate, actual (m <sup>3</sup> /hr)	342,717	324,552	308,016	325,095
Q <sub>s</sub>	Volumetric flow rate, standard (m <sup>3</sup> /hr)	231,315	221,009	231,386	227,903
Q <sub>std</sub>	Volumetric flow rate, dry standard (dry m <sup>3</sup> /hr)	175,443	165,605	173,845	171,631
Q <sub>std7</sub>	Volumetric flow rate, dry std @ 7% O <sub>2</sub> (dry m <sup>3</sup> /hr)	145,151	137,011	141,328	141,163
Q <sub>a</sub>	Volumetric flow rate, normal (Nm <sup>3</sup> /hr)	215,543	205,940	215,610	212,365
Q <sub>std</sub>	Volumetric flow rate, dry normal (Nm <sup>3</sup> /hr)	163,481	154,314	161,992	159,929
Q <sub>std7</sub>	Volumetric flow rate, dry normal @ 7% O <sub>2</sub> (Nm <sup>3</sup> /hr)	135,254	127,669	131,692	131,538
<b>Sampling Data</b>					
V <sub>std</sub>	Volume metered, standard (dscf)	85.9190	82.9102	81.9842	83.6045
%I	Isokinetic sampling (%)	102.6093	104.8983	98.8098	102.1058
<b>Laboratory Data</b>					
m <sub>n-1b</sub>	Fraction 1B Prorated (µg)	<0.1000	<0.1000	<0.1000	<0.1000
m <sub>n-2b</sub>	Fraction 2B Prorated (µg)	10.0180	10.9757	12.8701	11.2879
m <sub>n-3a</sub>	Fraction 3A Prorated (µg)	<0.2000	<0.2000	<0.2000	<0.2000
m <sub>n-3b</sub>	Fraction 3B Prorated (µg)	<0.5000	<0.5000	<0.5000	<0.5000
m <sub>n-3c</sub>	Fraction 3C Prorated (µg)	0.8182	<0.4000	<0.4000	<0.5394
m <sub>n</sub>	Total matter corrected for allowable blanks (µg)	10.8362	10.9757	12.8701	11.5607
<b>Mercury Results - Total</b>					
C <sub>sd</sub>	Concentration (lb/dscf)	2.7810E-10	2.9190E-10	3.4615E-10	3.0538E-10
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (lb/dscf)	3.3614E-10	3.5282E-10	4.2579E-10	3.7158E-10
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (lb/dscf)	3.4762E-10	3.5743E-10	4.4189E-10	3.8231E-10
C <sub>s</sub>	Concentration (lb/acf)	1.4236E-10	1.4894E-10	1.9537E-10	1.6222E-10
C <sub>sd</sub>	Concentration (µg/dscm)	4.4533E+00	4.6744E+00	5.5431E+00	4.8903E+00
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (µg/dscm)	5.3827E+00	5.6499E+00	6.8185E+00	5.9504E+00
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (µg/dscm)	5.5667E+00	5.7237E+00	7.0763E+00	6.1222E+00
C <sub>sd</sub>	Concentration (mg/dscm)	4.4533E-03	4.6744E-03	5.5431E-03	4.8903E-03
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (mg/dscm)	5.3827E-03	5.6499E-03	6.8185E-03	5.9504E-03
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (mg/dscm)	5.5667E-03	5.7237E-03	7.0763E-03	6.1222E-03
C <sub>a</sub>	Concentration (µg/m <sup>3</sup> (actual,wet))	2.2797E+00	2.3851E+00	3.1285E+00	2.5978E+00
C <sub>sd</sub>	Concentration (µg/Nm <sup>3</sup> dry)	4.7792E+00	5.0164E+00	5.9487E+00	5.2481E+00
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (µg/Nm <sup>3</sup> dry)	5.7766E+00	6.0633E+00	7.3174E+00	6.3858E+00
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (µg/Nm <sup>3</sup> dry)	5.9740E+00	6.1425E+00	7.5940E+00	6.5702E+00
E <sub>lb/hr</sub>	Rate (lb/hr)	1.7228E-03	1.7069E-03	2.1248E-03	1.8515E-03
E <sub>g/s</sub>	Rate (g/s)	2.1703E-04	2.1503E-04	2.6768E-04	2.3324E-04
E <sub>Tyr</sub>	Rate (Ton/yr)	7.5458E-03	7.4761E-03	9.3067E-03	8.1095E-03
E <sub>Fd</sub>	Rate - Fd-based (lb/MMBtu)	4.8368E-06	5.0768E-06	6.1269E-06	5.3468E-06
E <sub>Fc</sub>	Rate - Fc-based (lb/MMBtu)	5.2723E-06	5.4210E-06	6.7020E-06	5.7984E-06

Prepared by Clean Air Engineering, Inc. SS Metals-1 Version 10-2003

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USEPA Method 29  
 Mercury (Hg) Emission Parameters (continued)  
 Separate Front Half Results

Run No.	1	2	3	Average
Date (2005)	Sep 20	Sep 20	Sep 20	
Start Time (approx.)	08:30	12:04	14:35	
Stop Time (approx.)	11:18	14:17	16:50	

Mercury Results - Front Half

C <sub>sd</sub>	Concentration (lb/dscf)	<2.5664E-12	<2.6595E-12	<2.6895E-12	<2.6385E-12
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (lb/dscf)	<3.1020E-12	<3.2145E-12	<3.3084E-12	<3.2083E-12
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (lb/dscf)	<3.2080E-12	<3.2565E-12	<3.4335E-12	<3.2993E-12
C <sub>a</sub>	Concentration (lb/acf)	<1.3138E-12	<1.3570E-12	<1.5180E-12	<1.3963E-12
C <sub>sd</sub>	Concentration (µg/dscm)	<4.1097E-02	<4.2588E-02	<4.3069E-02	<4.2251E-02
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (µg/dscm)	<4.9674E-02	<5.1476E-02	<5.2979E-02	<5.1376E-02
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (µg/dscm)	<5.1371E-02	<5.2149E-02	<5.4982E-02	<5.2834E-02
C <sub>sd</sub>	Concentration (mg/dscm)	<4.1097E-05	<4.2588E-05	<4.3069E-05	<4.2251E-05
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (mg/dscm)	<4.9674E-05	<5.1476E-05	<5.2979E-05	<5.1376E-05
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (mg/dscm)	<5.1371E-05	<5.2149E-05	<5.4982E-05	<5.2834E-05
C <sub>a</sub>	Concentration (µg/m <sup>3</sup> (actual,wet))	<2.1038E-02	<2.1731E-02	<2.4308E-02	<2.2359E-02
C <sub>sd</sub>	Concentration (µg/Nm <sup>3</sup> dry)	<4.4104E-02	<4.5704E-02	<4.6221E-02	<4.5343E-02
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<5.3308E-02	<5.5243E-02	<5.6856E-02	<5.5136E-02
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<5.5130E-02	<5.5965E-02	<5.9005E-02	<5.6700E-02
E <sub>lb/hr</sub>	Rate (lb/hr)	<1.5898E-05	<1.5551E-05	<1.6510E-05	<1.5987E-05
E <sub>g/s</sub>	Rate (g/s)	<2.0028E-06	<1.9591E-06	<2.0798E-06	<2.0139E-06
E <sub>Tyr</sub>	Rate (Ton/yr)	<6.9635E-05	<6.8115E-05	<7.2313E-05	<7.0021E-05
E <sub>Fd</sub>	Rate - Fd-based (lb/MMBtu)	<4.4635E-08	<4.6255E-08	<4.7606E-08	<4.6165E-08
E <sub>Fc</sub>	Rate - Fc-based (lb/MMBtu)	<4.8654E-08	<4.9391E-08	<5.2074E-08	<5.0040E-08

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Wheelabrator North Broward, Inc  
 Clean Air Project No: 9708  
 Unit 3 FF Outlet

**USEPA Method 29  
 Mercury (Hg) Emission Parameters (continued)  
 Separate Impinger 1-3 Results**

Run No.	1	2	3	Average
Date (2005)	Sep 20	Sep 20	Sep 20	
Start Time (approx.)	08:30	12:04	14:35	
Stop Time (approx.)	11:18	14:17	16:50	

**Mercury Results - Impingers 1-3 Solution**

C <sub>sd</sub>	Concentration (lb/dscf)	2.5710E-10	2.9190E-10	3.4615E-10	2.9838E-10
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (lb/dscf)	3.1076E-10	3.5282E-10	4.2579E-10	3.6312E-10
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (lb/dscf)	3.2137E-10	3.5743E-10	4.4189E-10	3.7356E-10
C <sub>a</sub>	Concentration (lb/acf)	1.3161E-10	1.4894E-10	1.9537E-10	1.5864E-10
C <sub>sd</sub>	Concentration (µg/dscm)	4.1171E+00	4.6744E+00	5.5431E+00	4.7782E+00
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (µg/dscm)	4.9763E+00	5.6499E+00	6.8185E+00	5.8149E+00
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (µg/dscm)	5.1464E+00	5.7237E+00	7.0763E+00	5.9821E+00
C <sub>sd</sub>	Concentration (mg/dscm)	4.1171E-03	4.6744E-03	5.5431E-03	4.7782E-03
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (mg/dscm)	4.9763E-03	5.6499E-03	6.8185E-03	5.8149E-03
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (mg/dscm)	5.1464E-03	5.7237E-03	7.0763E-03	5.9821E-03
C <sub>a</sub>	Concentration (µg/m <sup>3</sup> (actual,wet))	2.1076E+00	2.3851E+00	3.1285E+00	2.5404E+00
C <sub>sd</sub>	Concentration (µg/Nm <sup>3</sup> dry)	4.4183E+00	5.0164E+00	5.9487E+00	5.1278E+00
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (µg/Nm <sup>3</sup> dry)	5.3404E+00	6.0633E+00	7.3174E+00	6.2404E+00
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (µg/Nm <sup>3</sup> dry)	5.5229E+00	6.1425E+00	7.5940E+00	6.4198E+00
E <sub>lb/hr</sub>	Rate (lb/hr)	1.5927E-03	1.7069E-03	2.1248E-03	1.8081E-03
E <sub>g/s</sub>	Rate (g/s)	2.0064E-04	2.1503E-04	2.6768E-04	2.2778E-04
E <sub>T/yr</sub>	Rate (Ton/yr)	6.9760E-03	7.4761E-03	9.3067E-03	7.9196E-03
E <sub>Fd</sub>	Rate - Fd-based (lb/MMBtu)	4.4716E-06	5.0768E-06	6.1269E-06	5.2251E-06
E <sub>Fc</sub>	Rate - Fc-based (lb/MMBtu)	4.8742E-06	5.4210E-06	6.7020E-06	5.6657E-06

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Wheelabrator North Broward, Inc  
 Clean Air Project No: 9708  
 Unit 3 FF Outlet

**USEPA Method 29  
 Mercury (Hg) Emission Parameters (continued)  
 Separate Impinger 4 Results**

Run No.		1	2	3	Average
Date (2005)		Sep 20	Sep 20	Sep 20	
Start Time (approx.)		08:30	12:04	14:35	
Stop Time (approx.)		11:18	14:17	16:50	
<b>Mercury Results - Impinger 4 Solution</b>					
C <sub>sd</sub>	Concentration (lb/dscf)	<5.1327E-12	<5.3190E-12	<5.3791E-12	<5.2769E-12
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (lb/dscf)	<6.2039E-12	<6.4291E-12	<6.6168E-12	<6.4166E-12
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (lb/dscf)	<6.4159E-12	<6.5131E-12	<6.8669E-12	<6.5986E-12
C <sub>a</sub>	Concentration (lb/acf)	<2.6275E-12	<2.7141E-12	<3.0360E-12	<2.7925E-12
C <sub>sd</sub>	Concentration (µg/dscm)	<8.2194E-02	<8.5176E-02	<8.6139E-02	<8.4503E-02
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (µg/dscm)	<9.9347E-02	<1.0295E-01	<1.0596E-01	<1.0275E-01
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (µg/dscm)	<1.0274E-01	<1.0430E-01	<1.0996E-01	<1.0567E-01
C <sub>sd</sub>	Concentration (mg/dscm)	<8.2194E-05	<8.5176E-05	<8.6139E-05	<8.4503E-05
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (mg/dscm)	<9.9347E-05	<1.0295E-04	<1.0596E-04	<1.0275E-04
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (mg/dscm)	<1.0274E-04	<1.0430E-04	<1.0996E-04	<1.0567E-04
C <sub>a</sub>	Concentration (µg/m <sup>3</sup> (actual,wet))	<4.2076E-02	<4.3462E-02	<4.8617E-02	<4.4718E-02
C <sub>sd</sub>	Concentration (µg/Nm <sup>3</sup> dry)	<8.8208E-02	<9.1409E-02	<9.2441E-02	<9.0686E-02
C <sub>sd7</sub>	Concentration @7% O <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<1.0662E-01	<1.1049E-01	<1.1371E-01	<1.1027E-01
C <sub>sd12</sub>	Concentration @12% CO <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<1.1026E-01	<1.1193E-01	<1.1801E-01	<1.1340E-01
E <sub>lb/hr</sub>	Rate (lb/hr)	<3.1797E-05	<3.1103E-05	<3.3019E-05	<3.1973E-05
E <sub>g/s</sub>	Rate (g/s)	<4.0056E-06	<3.9182E-06	<4.1597E-06	<4.0278E-06
E <sub>T/yr</sub>	Rate (Ton/yr)	<1.3927E-04	<1.3623E-04	<1.4463E-04	<1.4004E-04
E <sub>Fd</sub>	Rate - Fd-based (lb/MMBtu)	<8.9271E-08	<9.2510E-08	<9.5211E-08	<9.2331E-08
E <sub>Fc</sub>	Rate - Fc-based (lb/MMBtu)	<9.7308E-08	<9.8782E-08	<1.0415E-07	<1.0008E-07

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Wheelabrator North Broward, Inc  
 Clean Air Project No: 9708  
 Unit 3 FF Outlet

**USEPA Method 29  
 Mercury (Hg) Emission Parameters (continued)  
 Separate Impinger 5-6 Results**

Run No.	1	2	3	Average
Date (2005)	Sep 20	Sep 20	Sep 20	
Start Time (approx.)	08:30	12:04	14:35	
Stop Time (approx.)	11:18	14:17	16:50	

**Mercury Results - Filtered Permanganate Solution**

C <sub>sd</sub>	Concentration (lb/dscf)	<1.2832E-11	<1.3298E-11	<1.3448E-11	<1.3192E-11
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (lb/dscf)	<1.5510E-11	<1.6073E-11	<1.6542E-11	<1.6041E-11
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (lb/dscf)	<1.6040E-11	<1.6283E-11	<1.7167E-11	<1.6497E-11
C <sub>s</sub>	Concentration (lb/acf)	<6.5689E-12	<6.7851E-12	<7.5899E-12	<6.9813E-12
C <sub>sd</sub>	Concentration (µg/dscm)	<2.0548E-01	<2.1294E-01	<2.1535E-01	<2.1126E-01
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (µg/dscm)	<2.4837E-01	<2.5738E-01	<2.6490E-01	<2.5688E-01
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (µg/dscm)	<2.5686E-01	<2.6074E-01	<2.7491E-01	<2.6417E-01
C <sub>sd</sub>	Concentration (mg/dscm)	<2.0548E-04	<2.1294E-04	<2.1535E-04	<2.1126E-04
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (mg/dscm)	<2.4837E-04	<2.5738E-04	<2.6490E-04	<2.5688E-04
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (mg/dscm)	<2.5686E-04	<2.6074E-04	<2.7491E-04	<2.6417E-04
C <sub>s</sub>	Concentration (µg/m <sup>3</sup> (actual,wet))	<1.0519E-01	<1.0865E-01	<1.2154E-01	<1.1180E-01
C <sub>sd</sub>	Concentration (µg/Nm <sup>3</sup> dry)	<2.2052E-01	<2.2852E-01	<2.3110E-01	<2.2672E-01
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<2.6654E-01	<2.7621E-01	<2.8428E-01	<2.7568E-01
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (µg/Nm <sup>3</sup> dry)	<2.7565E-01	<2.7982E-01	<2.9503E-01	<2.8350E-01
E <sub>lb/hr</sub>	Rate (lb/hr)	<7.9492E-05	<7.7757E-05	<8.2549E-05	<7.9933E-05
E <sub>g/s</sub>	Rate (g/s)	<1.0014E-05	<9.7956E-06	<1.0399E-05	<1.0070E-05
E <sub>Ton/yr</sub>	Rate (Ton/yr)	<3.4817E-04	<3.4058E-04	<3.6156E-04	<3.5010E-04
E <sub>Fd</sub>	Rate - Fd-based (lb/MMBtu)	<2.2318E-07	<2.3128E-07	<2.3803E-07	<2.3083E-07
E <sub>Fc</sub>	Rate - Fc-based (lb/MMBtu)	<2.4327E-07	<2.4695E-07	<2.6037E-07	<2.5020E-07

**Mercury Results - HCl Rinse + HCl/MnO2 Precipitate**

C <sub>sd</sub>	Concentration (lb/dscf)	2.0998E-11	<1.0638E-11	<1.0758E-11	<1.4131E-11
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (lb/dscf)	2.5380E-11	<1.2858E-11	<1.3234E-11	<1.7157E-11
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (lb/dscf)	2.6247E-11	<1.3026E-11	<1.3734E-11	<1.7669E-11
C <sub>s</sub>	Concentration (lb/acf)	1.0749E-11	<5.4281E-12	<6.0720E-12	<7.4164E-12
C <sub>sd</sub>	Concentration (µg/dscm)	3.3625E-01	<1.7035E-01	<1.7228E-01	<2.2629E-01
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (µg/dscm)	4.0643E-01	<2.0590E-01	<2.1192E-01	<2.7475E-01
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (µg/dscm)	4.2032E-01	<2.0860E-01	<2.1993E-01	<2.8295E-01
C <sub>sd</sub>	Concentration (mg/dscm)	3.3625E-04	<1.7035E-04	<1.7228E-04	<2.2629E-04
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (mg/dscm)	4.0643E-04	<2.0590E-04	<2.1192E-04	<2.7475E-04
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (mg/dscm)	4.2032E-04	<2.0860E-04	<2.1993E-04	<2.8295E-04
C <sub>s</sub>	Concentration (µg/m <sup>3</sup> (actual,wet))	1.7213E-01	<8.6924E-02	<9.7234E-02	<1.1876E-01
C <sub>sd</sub>	Concentration (µg/Nm <sup>3</sup> dry)	3.6086E-01	<1.8282E-01	<1.8488E-01	<2.4285E-01
C <sub>sd7</sub>	Concentration @ 7% O <sub>2</sub> (µg/Nm <sup>3</sup> dry)	4.3617E-01	<2.2097E-01	<2.2742E-01	<2.9485E-01
C <sub>sd12</sub>	Concentration @ 12% CO <sub>2</sub> (µg/Nm <sup>3</sup> dry)	4.5107E-01	<2.2386E-01	<2.3602E-01	<3.0365E-01
E <sub>lb/hr</sub>	Rate (lb/hr)	1.3008E-04	<6.2206E-05	<6.6039E-05	<8.6108E-05
E <sub>g/s</sub>	Rate (g/s)	1.6387E-05	<7.8365E-06	<8.3193E-06	<1.0848E-05
E <sub>Ton/yr</sub>	Rate (Ton/yr)	5.6975E-04	<2.7246E-04	<2.8925E-04	<3.7715E-04
E <sub>Fd</sub>	Rate - Fd-based (lb/MMBtu)	3.6521E-07	<1.8502E-07	<1.9042E-07	<2.4688E-07
E <sub>Fc</sub>	Rate - Fc-based (lb/MMBtu)	3.9809E-07	<1.9756E-07	<2.0830E-07	<2.6798E-07

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Wheelabrator North Broward, Inc  
 Clean Air Project No: 9708  
 Unit 3 FF Outlet

**USEPA Method 29 (Mercury)  
 Sampling, Velocity and Moisture Parameters**

Run No.	4	5	6	Average	
Date (2005)	Sep 21	Sep 21	Sep 21		
Start Time (approx.)	08:05	10:43	13:15		
Stop Time (approx.)	10:20	12:59	15:29		
<b>Sampling Conditions</b>					
$Y_d$	Dry gas meter correction factor	0.9870	0.9870	0.9870	
$C_p$	Pitot tube coefficient	0.84	0.84	0.84	
$P_o$	Static pressure (in. H <sub>2</sub> O)	-12.5000	-12.5000	-12.3000	
$A_s$	Sample location area (ft <sup>2</sup> )	64.0000	64.0000	64.0000	
$P_{bar}$	Barometric pressure (in. Hg)	30.50	30.50	30.50	30.5000
$D_n$	Nozzle diameter (in.)	0.2760	0.2760	0.2760	
$O_2$	Oxygen (dry volume %)	10.2000	10.0000	10.2000	10.1333
$CO_2$	Carbon dioxide (dry volume %)	9.2000	9.2000	9.2000	9.2000
$N_2+CO$	Nitrogen plus carbon monoxide (dry volume %)	80.6000	80.8000	80.6000	80.6667
$V_{lc}$	Total Liquid collected (ml)	514.50	478.00	488.00	
$V_m$	Volume metered, meter conditions (ft <sup>3</sup> )	94.0750	85.9000	86.3800	
$T_m$	Dry gas meter temperature (°F)	91.2400	93.9600	97.3200	
$T_s$	Sample temperature (°F)	306.3600	305.7200	307.8800	306.6533
$\Delta H$	Meter box orifice pressure drop (in. H <sub>2</sub> O)	1.8012	1.4640	1.4956	
$\theta$	Total sampling time (min)	125.0	125.0	125.0	
<b>Flow Results</b>					
$V_{wstd}$	Volume of water collected (ft <sup>3</sup> )	24.2175	22.4995	22.9702	23.2290
$V_{mstd}$	Volume metered, standard (dscf)	91.0187	82.6343	82.6014	85.4181
$P_s$	Sample gas pressure, absolute (in. Hg)	29.5809	29.5809	29.5956	29.5858
$P_v$	Vapor pressure, actual (in. Hg)	29.5809	29.5809	29.5956	29.5858
$B_{wo}$	Moisture measured in sample (% by volume)	21.0155	21.4008	21.7579	21.3914
$B_{ws}$	Saturated moisture content (% by volume)	100.0000	100.0000	100.0000	100.0000
$B_w$	Actual water vapor in gas (% by volume)	21.0155	21.4008	21.7579	21.3914
$\sqrt{\Delta P}$	Velocity head ( $\sqrt{\text{in. H}_2\text{O}}$ )	0.7667	0.6947	0.6957	0.7190
$M_d$	MW of sample gas, dry (lb/lb-mole)	29.8800	29.8720	29.8800	29.8773
$M_s$	MW of sample gas, wet (lb/lb-mole)	27.3834	27.3313	27.2952	27.3366
$V_s$	Velocity of sample (ft/sec)	53.5514	48.5494	48.7093	50.2700
%I	Isokinetic sampling (%)	101.4417	101.9984	102.3239	101.9213
$Q_a$	Volumetric flow rate, actual (acfm)	205,637	186,430	187,044	193,037
$Q_s$	Volumetric flow rate, standard (scfm)	140,072	127,095	127,218	131,462
$Q_{std}$	Volumetric flow rate, dry standard (dscfm)	110,635	99,896	99,538	103,356
$Q_{std7}$	Volumetric flow rate, dry std@7%O <sub>2</sub> (dscfm)	85,165	78,335	76,623	80,041
$Q_a$	Volumetric flow rate, actual (acf/hr)	12,338,236	11,185,784	11,222,632	11,582,217
$Q_s$	Volumetric flow rate, standard (scf/hr)	8,404,342	7,625,703	7,633,095	7,887,713
$Q_{std}$	Volumetric flow rate, dry standard (dscf/hr)	6,638,124	5,993,742	5,972,293	6,201,386
$Q_a$	Volumetric flow rate, actual (m <sup>3</sup> /hr)	349,426	316,788	317,832	328,015
$Q_s$	Volumetric flow rate, standard (m <sup>3</sup> /hr)	238,016	215,964	216,174	223,385
$Q_{std}$	Volumetric flow rate, dry standard (dry m <sup>3</sup> /hr)	187,996	169,746	169,139	175,627
$Q_{std7}$	Volumetric flow rate, dry std@7%O <sub>2</sub> (dry m <sup>3</sup> /hr)	144,716	133,110	130,200	136,009
$Q_s$	Volumetric flow rate, normal (Nm <sup>3</sup> /hr)	221,788	201,240	201,435	208,154
$Q_{std}$	Volumetric flow rate, dry normal (Nm <sup>3</sup> /hr)	175,178	158,173	157,607	163,652
$Q_{std7}$	Volumetric flow rate, dry normal @7%O <sub>2</sub> (Nm <sup>3</sup> /hr)	134,849	124,035	121,323	126,736

Comments:

Average includes 3 runs.

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WHEELABRATOR NORTH BROWARD  
POMPANO BEACH, FLORIDA

Client Reference No: 14500124  
CleanAir Project No: 9708-4

**CALIBRATION DATA**

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Wheelabrator North Broward, Inc  
 Clean Air Project No: 9708  
 Unit 3 FF Outlet

**USEPA Method 29 (Mercury)  
 QA/QC Results**

Run No.	1	2	3
Date (2005)	Sep 20	Sep 20	Sep 20
Start Time (approx.)	08:30	12:04	14:35
Stop Time (approx.)	11:18	14:17	16:50
Total Duration of Test Run (min.)	168	133	135
Net Sampling Time (min.)	125	125	125

**Sampling System Calibration Summary**

$U_n$	Nozzle ID No:	.276-1	.276-1	.276-1
	Nozzle Diameter (in):	0.276	0.276	0.276
$U_p$	Probe ID No:	M-8-2	M-8-2	M-8-2
	Pitot Coefficient:	0.84	0.84	0.84
$Y_d$	Meter Box ID. No:	66-13	66-13	66-13
	Meter Box Yd - Field Sheet	0.9870	0.9870	0.9870
	Meter Box Yd - Database	0.9870	0.9870	0.9870
	Meter Box $\Delta H@$ - Field Sheet	1.7991	1.7991	1.7991
	Meter Box $\Delta H@$ - Database	1.7991	1.7991	1.7991

**QA/QC**

**Final Leak Check**

(a) 4% of Sampling Rate (cfm)	0.0289	0.0277	0.0277
(b) Allowable Rate from Method (cfm)	0.0200	0.0200	0.0200
Allowable Limit - minimum of a and b (cfm)	0.0200	0.0200	0.0200
Actual Final Leak Rate (cfm)	0.0050	0.0030	0.0030

**Sample Volume**

$V_{msd}$	Minimum Volume Required (dscf)	60.00	60.00	60.00
	Actual Sample Volume (dscf)	85.92	82.91	81.98

**Alternative Method 5 Post-Test Calibration (EPA ALT-009)**

$\sqrt{\Delta H_{avg}}$	Average of square root of $\Delta H$ (in. w.c.)	1.286	1.225	1.218
	Alternative Meter Calibration Factor	0.9969	0.9872	0.9894
$Y_{qa}$	Variation from full-test $Y_d$ (average $\leq \pm 5\%$ )	-1.0%	0.0%	-0.2%

Average  
-0.4%

**Mean Isokinetic Sampling Rate Variation**

%	Minimum Allowable (%)	90	90	90
	Maximum Allowable (%)	110	110	110
	Actual Variation (%)	102.61	104.90	98.81

**Point-by-Point Isokinetic Variation**

Number of points <90%	0	0	0
Number of points >110%	0	0	0
Number of points <80%	0	0	0
Number of points >120%	0	0	0

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# Nozzle Calibration Sheet

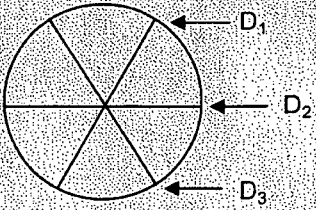
Client <u>WHEELABRATOR</u>	Project Number <u>9708</u>
Calibrated by <u>D DESIA</u>	Unit <u>3</u>
Date <u>7/20/05</u>	Runs <u>ALL</u>

Nozzle Identification	D <sub>1</sub> (inches)	D <sub>2</sub> (inches)	D <sub>3</sub> (inches)	ΔD (inches)	D <sub>ave</sub> (inches)
<u>.275-1</u>	<u>0.275</u>	<u>0.275</u>	<u>0.275</u>	<u>0.000</u>	<u>0.275</u>

D<sub>1</sub>, D<sub>2</sub>, D<sub>3</sub> = three nozzle diameter measurements

ΔD = maximum difference between any two diameters  
ΔD = 0.004 inches\*

D<sub>ave</sub> = average of D<sub>1</sub>, D<sub>2</sub>, D<sub>3</sub>



\* (40 CFR 60, Appendix A, Method 5, Section 5.1)

# Meter Box Full Test Calibration

Meter Box No: 66-13

Date of Calibration: 12/9/04

Meter Box  $Y_d$ : 0.9870

Calibration conducted by: M. V.

Meter Box  $\Delta H @$ : 1.7991

*M. V. [Signature]*  
Signature

Barometric Pressure: 29.05

				Standard Meter Gas Volume (ft <sup>3</sup> )			Meter Box Gas Volume (ft <sup>3</sup> )			Std. Meter Temperature (°F)			Meter Box Temperature (°F)			Time (min.)	Calibration Results	
Q	$\Delta H$	$\Delta P$	$Y_{ds}$	Initial	Final	$V_{ds}$ Net	Initial	Final	$V_d$ Net	In	Out	$T_{ds}$ Avg.	In	Out	Avg.	$\Theta$	$Y_d$	$\Delta H @$
0.936	3.00	-1.80	1.0000	0.000	10.000	10.000	637.925	648.258	10.333	66.0	66.0	66.00	91.0	70.0	80.50	10.41	0.9825	1.8636
0.936	3.00	-1.80	1.0000	0.000	10.000	10.000	648.258	658.575	10.317	66.0	66.0	66.00	91.0	70.0	80.50	10.41	0.9840	1.8636
0.395	0.50	-1.10	1.0000	0.000	5.000	5.000	661.920	667.048	5.128	66.0	66.0	66.00	82.0	70.0	76.00	12.32	0.9896	1.7402
0.396	0.50	-1.10	1.0000	0.000	5.000	5.000	667.048	672.171	5.123	66.0	66.0	66.00	82.0	70.0	76.00	12.31	0.9905	1.7373
0.676	1.50	-1.30	1.0000	0.000	10.000	10.000	676.066	686.336	10.270	66.0	66.0	66.00	87.0	68.0	77.50	14.41	0.9880	1.7923
0.675	1.50	-1.30	1.0000	0.000	10.000	10.000	686.336	696.611	10.275	66.0	66.0	66.00	87.0	68.0	77.50	14.43	0.9875	1.7972

Averages 0.98700 1.79905

Nomenclature	Equations
<p><math>P_b</math> Barometric Pressure (in. Hg)</p> <p><math>Q</math> Flow Rate (cfm)</p> <p><math>\Delta H</math> Orifice Pressure differential (in. H<sub>2</sub>O)</p> <p><math>\Delta P</math> Inlet Pressure Differential (in. H<sub>2</sub>O)</p> <p><math>V_d</math> Gas Meter Volume - Dry (ft<sup>3</sup>)</p> <p><math>V_{ds}</math> Standard Meter Volume - Dry (ft<sup>3</sup>)</p> <p><math>T_d</math> Average Meter Box Temperature (°F)</p> <p><math>T_o</math> Outlet Meter Box Temperature (°F)</p> <p><math>T_{ds}</math> Average Standard Meter Temperature (°F)</p> <p><math>Y_d</math> Meter Correction Factor (unitless)</p> <p><math>Y_{ds}</math> Standard Meter Correction Factor (unitless)</p> <p><math>\Delta H @</math> Orifice Pressure Differential giving 0.75 cfm of air at 68°F and 29.92 in. Hg (in. H<sub>2</sub>O)</p> <p><math>\Theta</math> Duration of Run (minutes)</p>	$Y_d = (Y_{ds}) \left[ \frac{V_{ds}}{V_d} \right] \left[ \frac{T_d + 460}{T_{ds} + 460} \right] \left[ \frac{P_b + \Delta P / 13.6}{P_b + \Delta H / 13.6} \right]$ $\Delta H @ = \frac{(0.0319)(\Delta H)}{P_b(T_o + 460)} \left[ \frac{(T_{ds} + 460)\Theta}{(V_{ds})(Y_{ds})} \right]^2$ $Q = \frac{17.64(V_{ds})(P_b)}{(T_{ds} + 460)(\Theta)}$

Vacuum Gauge		DGM Thermocouples		
Standard (in.Hg)	Gauge (in.Hg)	Standard (°F)	Inlet (°F)	Outlet (°F)
5.0	5.3			
10.0	10.4			
15.0	15.6			
20.0	20.3			
25.0	25.0			



## Pyrometer Calibration Test Report

Pyrometer No.:	<u>66-13</u>	Office:	<u>Palatine, IL</u>
Calibrated By:	<u>M. V.</u>	Client:	<u></u>
Date:	<u>12/9/04</u>	Job Number:	<u></u>

Calibration Reference Settings for Fahrenheit Scale	Pyrometer Reading
50 °F	49 °F
100 °F	98 °F
150 °F	149 °F
200 °F	200 °F
250 °F	251 °F
300 °F	300 °F
350 °F	350 °F
400 °F	399 °F
450 °F	448 °F
500 °F	498 °F
550 °F	549 °F
600 °F	600 °F

### Calibration Reference Information

Reference Used:	<u>Omega CL23A</u>	Serial No:	<u>T-225950</u>
Calibrated By:	<u>Omega Engineering, Inc.</u>	Exp.Date:	<u>9/15/05</u>
Report No:	<u>R 044791</u>		



### Meter Box Critical Orifice Post-Test Calibration Data

Project No. 9706/9708                      Meter No. 66-13                      Orifice A-4  
 Location Palatine Warehouse                      Meter Yd 0.9870                      Orifice K' 0.4930  
 Test Date 10/12/2005                      Meter ΔH@ 1.7991                      Orifice Cal. Date 9/28/2005  
 Operator P. Bihun                      Full Test Cal. Date 12/9/2004

Leak Checks

Negative Pressure  
 No movement of manometer in one-minute  Pass

Positive Pressure  
 No movement of manometer in one-minute  Pass

Important: All leak checks must pass in order for calibration to be valid.

Barom. Press. (P<sub>b</sub>) 29.50 in. Hg

Run	Elapsed Time (minutes)	Meter Volume (dcf)	Meter Temperature		Ambient Temp. T <sub>amb</sub> (°F)	Orifice ΔH (in. W.C.)	Vacuum (in. Hg)	Net Run Time - θ (minutes)	Net Meter Volume for Run - V <sub>m</sub> (dcf)	Avg. Meter Temp. for Run - T <sub>m</sub> (°F)	DGM Calibration Factor - Y <sub>i</sub>	Percent Variation - ΔY <sub>i</sub>
			Inlet (°F)	Outlet (°F)								
	0.0	811.900	70	68								
1	5.0	815.15	70	68	71	1.30	16.5	5.0	3.25	69.0	0.9839	-0.1%
2	10.0	818.40	71	68	71	1.30	16.5	5.0	3.25	69.3	0.9843	-0.1%
3	15.0	821.645	72	69	72	1.30	16.5	5.0	3.25	70.0	0.9863	0.2%

Average Y <sub>i</sub>	0.9848
Cal. Error	-0.2%

**Calculations and Specifications**

$$Y_i = \frac{K' \times P_b \times (T_m + 460) \times \theta}{17.64 \times V_m \times (P_b + \frac{\Delta H}{13.6}) \times \sqrt{T_{amb} + 460}}$$

$$\Delta Y_i = \frac{Y_i - \bar{Y}_i}{\bar{Y}_i} \times 100 \quad \text{Spec. : } \Delta Y_i \leq \pm 2\%$$

$$Cal. Error = \frac{\bar{Y}_i - Y_d}{Y_d} \times 100 \quad \text{Spec. : } Cal. Error \leq \pm 5\%$$

C - 7

## Meter Box Critical Orifice Post-Test Calibration Data

Project No. 970619708      Meter No. 66-13      Orifice A-4  
 Location Salina Fire Warehouse      Meter  $Y_d$  0.98700      Orifice  $K'$  0.4930  
 Test Date 10/12/05      Meter  $\Delta H_{@}$  1.79905      Orifice Cal. Date 9/28/05  
 Operator P. Bikun      Full Test Cal. Date 12/9/04

### Leak Checks

Negative Pressure <i>No movement of Manometer in one-minute</i>	<input checked="" type="checkbox"/> Pass <input type="checkbox"/> Fail
Positive Pressure <i>No movement of Manometer in one-minute</i>	<input checked="" type="checkbox"/> Pass <input type="checkbox"/> Fail

Important: All leak checks must pass in order for calibration to be valid.

Bar. Press. ( $P_b$ ) 29.50 in. Hg

Run	Elapsed Time (minutes)	Meter Volume (dcf)	Meter Temperature		Ambient Temp. $T_{amb}$ (°F)	Orifice $\Delta H$ (In. W.C.)	Vacuum (In. Hg)	Net Run Time - $\theta$ (minutes)	Net Meter Volume for Run - $V_m$ (dcf)	Avg Meter Temp. for Run - $T_m$ (°F)	DGM Calibration Factor $Y_i$	Percent Variation $\Delta Y_i$
			Inlet (°F)	Outlet (°F)								
	0	811.900	70	68								
1	5	815.15	70	68	71	1.3	16.5					
2	10	818.40	71	68	71	1.3	16.5					
3	15	821.645	72	69	72	1.3	16.5					

Average  $Y_i$

Cal. Error

### Calculations and Specifications

$$Y_i = \frac{K' \times P_b \times (T_m + 460) \times \theta}{17.64 \times V_m \times (P_b + \frac{\Delta H}{13.6}) \times \sqrt{T_{amb} + 460}}$$

$$\Delta Y_i = \frac{Y_i - \bar{Y}_i}{\bar{Y}_i} \times 100 \quad \text{Spec.: } \Delta Y_i \leq \pm 2\%$$

$$\text{Cal. Error} = \frac{\bar{Y}_i - Y_d}{Y_d} \times 100 \quad \text{Spec.: } \text{Cal. Error} \leq \pm 5\%$$



**SAMPLE PROBE CALIBRATION DATA**

Probe Type: M5 I.D. number: M-8-2

**Thermocouple Calibration**

Reference Type: \_\_\_\_\_ Reference I.D. No: \_\_\_\_\_ Pyrometer I.D. No: \_\_\_\_\_ Degrees: F / C

Point No.	Target Temp.	Reference Temp	Indicated Temp	Temp Difference	% Difference	Specification
1	ice-32°F					%Difference ≤ 1.5
2	ambient-70°F					
3	hot oil-150°F					
4	boiling H <sub>2</sub> O-212°F					
5	hot oil-320°F					

Does assembly meet specifications?  → If "NO" thermocouple must be replaced.

**Geometric Pitot Calibration** *diagrams on reverse*

Is pitot assembly in good repair?  YES / NO If "NO" explain: \_\_\_\_\_  
 If repairs are required, pitot does not meet specification.



**"S" Pitot**

Measurement		Specification
a1 = <u>1</u>	a2 = <u>2</u>	<10°
b1 = <u>1</u>	b2 = <u>2</u>	<5°
γ = <u>0</u>	θ = <u>2</u>	
Pa = <u>0.355</u>	Pb = <u>0.355</u>	Pa + Pb = A
A = <u>0.710</u>	Dt = <u>0.25</u>	
Calculations		
z = A sin γ = <u>0.000</u>		<0.125"
w = A sin θ = <u>0.02478</u>		<0.03125"

Does assembly meet specifications?

YES / NO



**Standard Pitot**

Measurement	Specification
Tube O.D. _____	(D)
Static Hole I.D. _____	0.1 x D =
Length, _____	
Tip to Static _____	> 6xD =
Static to Bend _____	> 8xD =

Does assembly meet specifications? YES / NO

If "YES" "S" pitot Cp=0.84; Std pitot Cp=0.99  
 If "NO" wind tunnel calibration is required.

**Wind Tunnel Pitot Calibration**

Reference Pitot I.D. No: \_\_\_\_\_ Reference Pitot Cp: \_\_\_\_\_

**Pitot Side 'A':**

Trial No.	Reference ΔP	Probe ΔP	Probe Cp*	Deviation from Average Cp*	Specification
1					Cp Deviations ≤ 0.01
2					
3					

Side 'A' Average Probe Cp= \_\_\_\_\_

**Pitot Side 'B':**

Trial No.	Reference ΔP	Probe ΔP	Probe Cp*	Deviation from Average Cp*	Specification
1					Cp Deviations ≤ 0.01
2					
3					

Side 'B' Average Probe Cp= \_\_\_\_\_

\* Probe Cp=(Reference Cp)√(Reference ΔP / Probe ΔP); Cp Deviation= Trial Probe Cp - Average Probe Cp

Side 'A' Average Cp \_\_\_\_\_ - Side 'B' Average Cp \_\_\_\_\_ = \_\_\_\_\_ Abs. Diff. ≤ 0.01

Does assembly meet specifications?  YES / NO → If "YES" Cp=Average of Side 'A' and 'B' Cp values.  
 If "NO" PITOT MUST BE REPLACED.

**All specifications are from EPA-600/9-76-005, section 3.1**

PROBE Cp = 0.84 Calibrated by: [Signature] Date: 2/24/05



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WHEELABRATOR NORTH BROWARD  
POMPANO BEACH, FLORIDA

Client Reference No: 14500124  
CleanAir Project No: 9708-4

**FIELD DATA**

**D**



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TEST LOCATION: FF Outlet

UNIT: 3

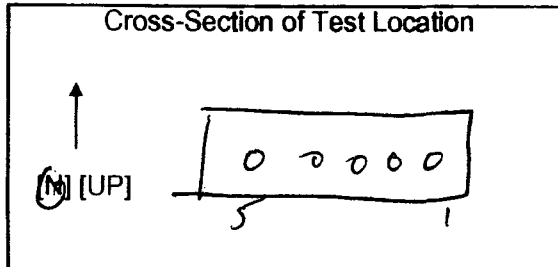
RUN: 1

Mercury TESTING  
FIELD DATA SHEET

METHOD: 29 PAGE 1 OF 2

Client <u>Wheelabrator</u>	Project No. <u>9708</u>
Plant <u>North Broward</u>	Date <u>9/20/05</u>
Meter Operator <u>PA</u>	
Probe Operator <u>PB</u>	

Meter Box <u>1010-13</u>	Sample Box No. <u>67-21</u>
Meter Y <sub>d</sub> <u>0.98700</u>	Meter ΔH <sub>0</sub> <u>1.79905</u>
K Factor <u>3.00</u>	Pitot C <sub>p</sub> <u>0.24</u>
Leak Rate Before <u>0.007</u> (cm <sup>3</sup> /Lpm) @ <u>15</u> (in. Hg)	
Leak Rate After <u>0.005</u> (cm <sup>3</sup> /Lpm) @ <u>9</u> (in. Hg)	
Pitot Leak Check Before: <input checked="" type="checkbox"/> After: Good <input checked="" type="checkbox"/> Bad <input type="checkbox"/>	



Duct Dimensions (in.) <u>96x96</u>			
Static Pres (in. H <sub>2</sub> O) <u>-11.1</u>	Port Len. (in.) <u>10</u>	Gas Flow (in) (Out) of page <u>(in) [Out]</u>	First point all the way <u>(in) [Out]</u>

Amb. Temp. (°F) <u>82</u>	Bar. Press. <u>30.00</u> (in. Hg) (mbar)
Probe I.D. No. <u>M-8-2</u>	
Liner Material <u>Glass</u>	

Filter No. <u>N/A</u>	
Thimble No. <u>N/A</u>	
Nozzle Diameter <u>0.224</u>	Nozzle I.D. <u>276-1</u>

Start Time: <u>8:30</u>	Stop Time: <u>11:18</u>
-------------------------	-------------------------

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. (ft <sup>3</sup> ) (L)	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)	Filter T <sub>f</sub> (°F)	Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>m in</sub> (°F)	DGM Outlet T <sub>m out</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>t</sub> (°F)	Notes
						Set Points							
1-1	5	28	1.84	755.410	295	250	250	66	82	81	2.5	N/A	
2	10	38	1.1	760.90	301	250	250	60	82	81	3.0		
3	15	50	1.5	764.32	307	250	250	54	85	81	3.5		
4	20	51	1.5	767.75	307	250	257	52	89	82	3.5		
5	25	56	1.7	771.395	307	250	252	52	91	83	4.0		(-0.115) 771.510
2-1	30	86	2.6	775.95	309	249	253	54	93	85	5.5		
2	35	68	2.0	779.92	309	244	247	51	95	85	4.5		
3	40	63	1.9	783.75	307	250	260	52	97	87	4.5		
4	45	58	1.7	787.42	307	250	246	54	97	87	4.0		
5	50	63	1.9	791.300	309	250	260	59	97	88	4.5		791.382
3-1	55	58	1.7	795.02	309	249	254	62	96	89	4.0		(-0.082) 795.02
2	60	74	2.2	799.13	308	250	251	60	97	89	5.0		
Total		9.03799		90.4630									
Average		0.7454	1.6736		303.040				92.2000				

Sum of square roots. 74373

Circle correct bracketed units on data sheet.

QA/QC D  
Date 9/20/05

2119



TEST LOCATION: FF Outlet  
 UNIT: 3 RUN: 1

Mercury TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 2 OF 2

Client <u>Wheelabrator</u>	Project No. <u>9708</u>
Plant <u>North Branch</u>	Date <u>9/20/05</u>
Meter Operator <u>PB</u>	
Probe Operator <u>PB</u>	

Meter Box	Sample Box No.
Meter Y <sub>d</sub>	Meter ΔH <sub>@</sub>
K Factor	Pitot C <sub>p</sub>
Leak Rate Before [cfm] [Lpm] @ (in. Hg)	
Leak Rate After [cfm] [Lpm] @ (in. Hg)	
Pitot Leak Check Before: <input type="checkbox"/> After: Good <input type="checkbox"/> Bad <input type="checkbox"/>	

Cross-Section of Test Location

↑  
[N] [UP]

Duct Dimensions (in.)

Static Pres (in. H <sub>2</sub> O)	Port Len. (in.)	Gas Flow [In] [Out] of page	First point all the way [In] [Out]
------------------------------------	-----------------	-----------------------------	------------------------------------

Amb. Temp. (°F) ^	Bar. Press. [in. Hg] [mbar]
Probe I.D. No.	
Liner Material	

Filter No.	
Thimble No.	
Nozzle Diameter	Nozzle I.D.

Start Time:	Stop Time:
-------------	------------

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. (ft <sup>3</sup> ) [L]	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)	Filter T <sub>f</sub> (°F)	Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>min</sub> (°F)	DGM Outlet T <sub>min</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>t</sub> (°F)	Notes
						Set Points							
						250	250						
3	65	167	2.0	803.15	309	250	261	51	99	90	4.5	W/A	
4	70	161	1.8	806.93	309	280	250	46	99	90	4.5		Pause @ 9:40
5	75	43	1.3	810.200	299	251	251	58	93	90	4.0		rotate @ 10:07
4-1	80	163	1.9	814.19	299	250	260	58	96	91	4.5		Leak ✓ wood
2	85	165	2.0	818.15	300	250	246	54	98	91	5.0		(0.120) 50.3
3	90	158	1.7	821.87	299	250	247	51	100	92	4.5		
4	95	150	1.5	825.32	296	250	261	54	101	93	4.0		
5	100	43	1.3	828.590	299	280	251	56	101	93	4.0		828.690
5-1	105	51	1.5	832.07	297	249	253	61	99	93	4.0		(-0.05)
2	110	55	1.7	835.80	299	250	260	57	101	94	4.5		
3	115	154	1.6	839.40	299	250	255	57	101	94	4.5		
4	120	151	1.5	842.86	297	250	253	58	102	94	4.5		
5	125	45	1.4	846.240	299	251	251	58	102	94	4.0		
	Total	9.5552											
	Average												

\*Sum of square roots.

Circle correct bracketed units on data sheet.

QA/QC 102  
 Date 9/20/05



D - 4

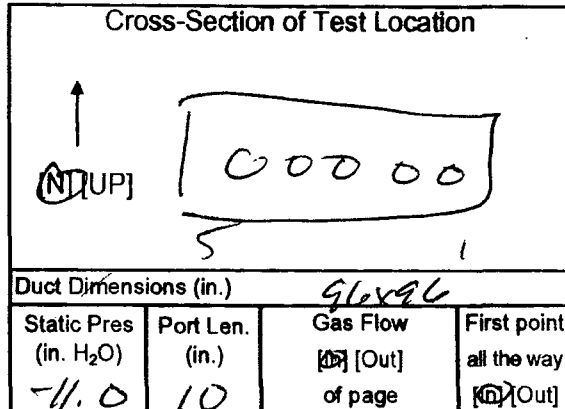
TEST LOCATION: FF Outlet  
 UNIT: 3 RUN: 2

Mercury TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 1 OF 2

Client Wheelabrator Project No. 9708  
 Plant North Broward Date 9/20/05  
 Meter Operator PB  
 Probe Operator PB

Meter Box 66-13 Sample Box No. 71-20  
 Meter Y<sub>d</sub> 6.98700 Meter ΔH<sub>0</sub> 1.7905  
 K Factor 3.00 Pitot C<sub>p</sub> 0.81  
 Leak Rate Before 0.006 [Lpm] @ 15 (in. Hg)  
 Leak Rate After 0.003 [Lpm] @ 9 (in. Hg)  
 Pitot Leak Check Before:  After: Good  Bad



Amb. Temp. (°F) 80 Bar. Press. 30.60 (in. Hg) [mbar]  
 Probe I.D. No. M-1-2  
 Liner Material Glass

Filter No. N/A  
 Thimble No. N/A  
 Nozzle Diameter 6.776 Nozzle I.D. 2.26-1

Start Time: 12:04 Stop Time: 14:17

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. (ft <sup>3</sup> )	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)	Filter T <sub>f</sub> (°F)	Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>min</sub> (°F)	DGM Outlet T <sub>min</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>t</sub> (°F)	Notes
						Set Points							
1-1	5	55	1.7	850.76	295	230	245	61	83	85	3.5	N/A	
2	10	53	1.6	854.32	292	250	243	50	85	85	3.5		
3	15	40	1.2	857.46	291	250	245	48	87	84	3.0		
4	20	53	1.6	861.07	297	280	251	49	88	84	3.5		
5	25	56	1.7	864.75	297	250	257	51	89	84	3.5		
1-1	30	68	2.0	868.74	298	244	242	56	88	83	4.0		868.810 -0.035
2	35	53	1.6	872.33	297	280	256	54	90	83	3.5		
3	40	48	1.4	875.68	297	280	251	55	90	83	3.5		
4	45	47	1.4	879.64	298	250	244	58	90	84	3.5		
5	50	42	1.3	882.270	297	280	256	60	90	84	3.5		
3-1	55	57	1.7	885.97	297	249	241	63	88	84	4.0		882.305
2	60	61	1.8	889.75	297	249	256	60	90	84	4.0		-0.035
Total		860.52											
Average		0.7074	1.5080	86.625	296.480			87.7400					

Sum of square roots.  
70633 19.0

Circle correct bracketed units on data sheet.  
 3553 QA/QC DR  
 Date 9/20/05

2068 86.60

TEST LOCATION: FF Outlet  
 UNIT: 3 RUN: 2

Mercury TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 2 OF 2

Client <u>Lehigh Valley</u>	Project No. <u>9708</u>
Plant <u>North Branch</u>	Date <u>9/20/05</u>
Meter Operator <u>PB</u>	
Probe Operator <u>AB</u>	

Meter Box	Sample Box No.
Meter Y <sub>d</sub>	Meter ΔH <sub>@</sub>
K Factor	Pitot C <sub>p</sub>
Leak Rate Before [cfm] [Lpm] @ (in. Hg)	
Leak Rate After [cfm] [Lpm] @ (in. Hg)	
Pitot Leak Check Before: <input type="checkbox"/> After: Good <input type="checkbox"/> Bad <input type="checkbox"/>	

Cross-Section of Test Location

↑  
[N] [UP]

Duct Dimensions (in.)

Static Pres (in. H <sub>2</sub> O)	Port Len. (in.)	Gas Flow (In) [Out]	First point all the way (In) [Out]
------------------------------------	-----------------	---------------------	------------------------------------

of page

Amb. Temp. (°F)	Bar. Press. (in. Hg) [mbar]
Probe I.D. No.	
Liner Material	

Filter No.	
Thimble No.	
Nozzle Diameter	Nozzle I.D.

Start Time:	Stop Time:
-------------	------------

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. [L]	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)		Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>m in</sub> (°F)	DGM Outlet T <sub>m out</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>i</sub> (°F)	Notes
						Set Points	Set Points						
3	65	.57	1.7	893.42	295	250	250	61	91	84	4.0		
4	70	.50	1.5	896.91	299	250	247	62	92	84	4.0		
5	75	.43	1.3	900.140	298	250	259	64	92	84	3.5		Leak ✓ ok
4-1	80	.58	1.7	903.89	296	250	258	65	89	85	4.0		900.250 -0.110
2	85	.59	1.8	907.71	297	250	252	63	92	85	4.0		
3	90	.51	1.5	911.17	297	250	244	61	93	85	3.5		
4	95	.47	1.4	914.51	297	250	245	63	94	86	3.5		
5	100	.38	1.1	917.460	297	250	255	60	94	86	3.0		
5-1	105	.42	1.3	920.73	296	249	243	62	91	86	3.5		917.515 -0.055
2	110	.44	1.3	923.95	297	250	259	59	93	87	3.5		
3	115	.45	1.4	927.32	297	251	251	59	95	88	4.0		
4	120	.48	1.4	930.166	296	251	253	58	95	88	4.0		
5	125	.42	1.3	933.905	297	250	259	58	95	88	3.5		
Total		8.90478											
Average													

\*Sum of square roots.

Circle correct bracketed units on data sheet.

QA/QC D2  
 Date 9/20/05



TEST LOCATION: FF Outlet

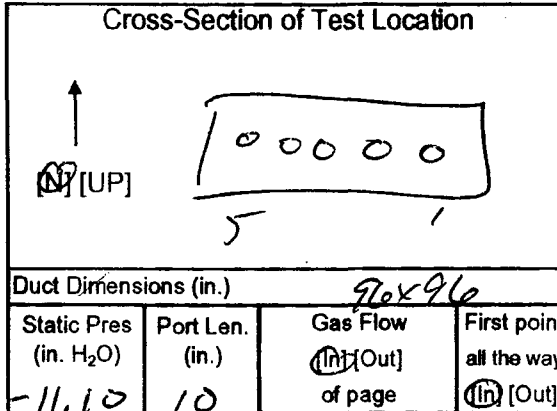
Mercury TESTING  
FIELD DATA SHEET

METHOD: 29 PAGE 1 OF 2

UNIT: 3 RUN: 3

Client <u>Wheeler</u>	Project No. <u>9708</u>
Plant <u>Nov H. Brewer</u>	Date <u>9/20/05</u>
Meter Operator <u>PA</u>	
Probe Operator <u>PA</u>	

Meter Box <u>106-13</u>	Sample Box No. <u>4727</u>
Meter <u>Yd 0.9x700</u>	Meter $\Delta H_0$ <u>1.7885</u>
K Factor	Pitot $C_p$ <u>0.04</u>
Leak Rate Before <u>0.004</u> [Lpm] @ <u>15</u> (in. Hg)	
Leak Rate After <u>0.003</u> [Lpm] @ <u>8</u> (in. Hg)	
Pitot Leak Check Before: <input checked="" type="checkbox"/> After: Good <input checked="" type="checkbox"/> Bad <input type="checkbox"/>	



Amb. Temp. (°F) <u>85</u>	Bar. Press. <u>30.05</u> (in. Hg) [mbar]
Probe I.D. No. <u>M-8-2</u>	
Liner Material <u>Galss</u>	

Filter No. <u>N/A</u>	
Thimble No. <u>N/A</u>	
Nozzle Diameter <u>0.276</u>	Nozzle I.D. <u>276-1</u>

Start Time: 14:35 Stop Time: 16:50

Traverse Point Number	Min/pt Elapsed Time	Velocity Head $\Delta P$ (in. H <sub>2</sub> O)	Orifice Setting $\Delta H$ (in. H <sub>2</sub> O)	Gas Sample Volume $V_m$ Init. Vol. [L]	Stack Temp. $T_s$ (°F)	Probe $T_p$ (°F)		Filter $T_f$ (°F)	Cond. Temp. $T_c$ (°F)	DGM Inlet $T_{min}$ (°F)	DGM Outlet $T_{out}$ (°F)	Pump Vacuum (in.Hg)	XAD Trap Temp. $T_t$ (°F)	Notes
						Set Points	Set Points							
	<u>5</u>	<u>.23</u>	<u>.69</u>	<u>934.180</u>		<u>252</u>	<u>252</u>							
1-1	<u>5</u>	<u>.23</u>	<u>.69</u>	<u>930.55</u>	<u>283</u>	<u>250</u>	<u>257</u>	<u>66</u>	<u>88</u>	<u>88</u>	<u>2.5</u>	<u>N/A</u>		
2	<u>10</u>	<u>.25</u>	<u>.75</u>	<u>939.01</u>	<u>284</u>	<u>280</u>	<u>260</u>	<u>48</u>	<u>90</u>	<u>88</u>	<u>2.5</u>			
3	<u>15</u>	<u>.37</u>	<u>.96</u>	<u>941.77</u>	<u>295</u>	<u>280</u>	<u>286</u>	<u>43</u>	<u>91</u>	<u>88</u>	<u>3.0</u>			
4	<u>20</u>	<u>.41</u>	<u>1.2</u>	<u>944.89</u>	<u>296</u>	<u>281</u>	<u>247</u>	<u>42</u>	<u>92</u>	<u>88</u>	<u>3.0</u>			
5	<u>25</u>	<u>.58</u>	<u>1.7</u>	<u>948.555</u>	<u>298</u>	<u>280</u>	<u>259</u>	<u>42</u>	<u>94</u>	<u>89</u>	<u>4.0</u>			
2-1	<u>30</u>	<u>.73</u>	<u>2.2</u>	<u>952.71</u>	<u>297</u>	<u>280</u>	<u>245</u>	<u>97</u>	<u>94</u>	<u>89</u>	<u>4.5</u>			<u>948.620</u>
2	<u>35</u>	<u>.66</u>	<u>2.0</u>	<u>956.68</u>	<u>300</u>	<u>281</u>	<u>253</u>	<u>44</u>	<u>96</u>	<u>89</u>	<u>4.5</u>			<u>-0.065</u>
3	<u>40</u>	<u>.57</u>	<u>1.7</u>	<u>960.41</u>	<u>298</u>	<u>280</u>	<u>259</u>	<u>46</u>	<u>97</u>	<u>90</u>	<u>4.0</u>			
4	<u>45</u>	<u>.51</u>	<u>1.5</u>	<u>963.91</u>	<u>296</u>	<u>280</u>	<u>248</u>	<u>47</u>	<u>97</u>	<u>90</u>	<u>4.0</u>			
5	<u>52</u>	<u>.47</u>	<u>1.4</u>	<u>967.260</u>	<u>297</u>	<u>280</u>	<u>260</u>	<u>49</u>	<u>96</u>	<u>90</u>	<u>4.0</u>			
3-1	<u>55</u>	<u>.53</u>	<u>1.6</u>	<u>970.86</u>	<u>297</u>	<u>280</u>	<u>249</u>	<u>56</u>	<u>94</u>	<u>90</u>	<u>4.0</u>			<u>962.295</u>
2	<u>60</u>	<u>.64</u>	<u>1.9</u>	<u>974.75</u>	<u>298</u>	<u>280</u>	<u>250</u>	<u>54</u>	<u>96</u>	<u>91</u>	<u>4.5</u>			<u>0.035</u>
	Total			<u>86.430</u>										
	Average	<u>0.7038</u>	<u>1.5080</u>	<u>964.57</u>	<u>294.5600</u>				<u>92.6800</u>					

Sum of square roots: 17.6  
 Circle correct bracketed units on data sheet.  
86.430  
9537 QA/QC 9/20/05  
 Date DR

D-7



TEST LOCATION: FF Outlet  
 UNIT: 3 RUN: 3

Mercury TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 2 OF 2

Client <u>Whisperba</u>	Project No. <u>9708</u>
Plant <u>North Branch</u>	Date <u>7/20/05</u>
Meter Operator <u>RB</u>	
Probe Operator <u>RB</u>	

Meter Box	Sample Box No.
Meter Y <sub>d</sub>	Meter ΔH <sub>@</sub>
K Factor	Pitot C <sub>p</sub>

Leak Rate Before	[cfm] [Lpm]	@	(in. Hg)
Leak Rate After	[cfm] [Lpm]	@	(in. Hg)
Pitot Leak Check Before:	<input type="checkbox"/>	After: Good	<input type="checkbox"/> Bad <input type="checkbox"/>

Cross-Section of Test Location

↑  
[N] [UP]

Duct Dimensions (in.)

Static Pres (in. H <sub>2</sub> O)	Port Len. (in.)	Gas Flow [In] [Out] of page	First point all the way [In] [Out]
------------------------------------	-----------------	-----------------------------	------------------------------------

Amb. Temp. (°F)	Bar. Press. [in. Hg] [mbar]
Probe I.D. No.	
Liner Material	

Filter No.	
Thimble No.	
Nozzle Diameter	Nozzle I.D.

Start Time:	Stop Time:
-------------	------------

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. [L]	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)	Filter T <sub>f</sub> (°F)	Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>min</sub> (°F)	DGM Outlet T <sub>out</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>t</sub> (°F)	Notes
						Set Points							
3	105	1.58	1.7	978.46	282 RB	250	252	53	97 RB	91	4.5		
4	70	1.50	1.5	981.97	301	250	254	59	97	91	4.0		
5	25	1.45	1.4	985.325	297	250	261	62	97	91	4.0		Leak of OK
4-1	80	1.62	1.9	989.31	296	250	258	64	93	91	4.5		
2	85	1.62	1.9	993.14	297	250	259	51	97	91	4.5		985.425
3	90	1.53	1.6	996.80	298	250	255	47	97	91	4.5		(-0.073)
4	95	1.53	1.6	1000.41	298	249	244	45	97	91	4.5		(-0.1)
5	100	1.48	1.4	1003.830	297	250	254	45	97	91	4.0		
5-1	105	1.48	1.4	1007.27	298	250	252	50	94	91	4.0		1002.890
2	110	1.53	1.6	1010.86	299	250	251	47	96	91	4.5		(-0.06)
3	115	1.53	1.6	1014.43	298	250	260	49	98	91	4.5		
4	120	1.48	1.4	1017.85	297	250	257	50	98	91	4.5		
5	125	1.38	1.4	1020.870	297	251	256	50	98	91	4.0		
Total													
Average													

\* Sum of square roots.

Circle correct bracketed units on data sheet.

QA/QC DR  
 Date 7/21/05



# ORSAT READINGS

TEST LOCATION: FF OUTLET UNIT 3

PAGE 1 OF 1

Client	WHEELABRATOR	Project Number	9708	$Fo = \frac{20.9 - \%O_2}{\%CO_2}$
Plant	NORTH	Unit	3	
Orsat ID	#3	Fuel Type	mw	Leak Check Passed <input checked="" type="checkbox"/>

Run Number	Method Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Fo	Analyst	Analysis	
								Date	Time
1	m29	1	9.6	19.0	9.4		D <sup>2</sup>	9/20	1254
		2	9.6	19.0	9.4				
		3	9.6	19.0	9.4				
		Avg	(9.6)		(9.4)				
2	m29	1	9.8	19.2	9.4		D <sup>2</sup>	9/20	1519
		2	9.8	19.2	9.4				
		3	9.8	19.2	9.4				
		Avg	(9.8)		(9.4)				
3	m29	1	9.4	19.0	9.6		D <sup>2</sup>	9/20	1735
		2	9.4	19.0	9.6				
		3	9.4	19.0	9.6				
		Avg	(9.4)		(9.6)				
		1							
		2							
		3							
		Avg							
		1							
		2							
		3							
		Avg							
		1							
		2							
		3							
		Avg							

Repeat the analysis procedure until the results of any three analyses differ by no more than 0.2 percent by volume. Average the three acceptable values and report the results to the nearest 0.1 percent. Calculate Fo to verify result.

Acceptable ranges for Fo:

Coal: Anthracite and lignite	1.016-1.130	Gas: Natural	1.600-1.836
Bituminous	1.083-1.230	Propane	1.434-1.586
Oil: Distillate	1.260-1.413	Butane	1.405-1.553
Residual	1.210-1.370	Wood:	1.000-1.120



# Impinger Weight Sheet

Client <u>WHEELABRATOR</u>	Unit Name / Location <u>3 FF OUTLET</u>
Plant <u>NORTH</u>	Job No. <u>9708</u> Method <u>29</u>

Run No. <u>1</u>	Filter Type <u>QUARTZ</u>	Sample Box No. <u>67-27</u>
Date <u>9/20/05</u>	Lot No. <u>D1441301</u>	pH <u>NA</u>
Analyst <u>D<sup>2</sup></u>	Filter No. <u>NA</u>	Rinse <u>NA</u>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)				
Impinger 1	<u>EMPTY</u>	<u>786.5</u>	<u>436.8</u>	<u>349.7</u>	<table border="1" style="width: 100%; border-collapse: collapse;"> <tr> <td>QA/QC <u>D<sup>2</sup></u></td> </tr> <tr> <td>Date <u>9/20</u></td> </tr> <tr> <td>Total Weight (gm)</td> </tr> </table>	QA/QC <u>D<sup>2</sup></u>	Date <u>9/20</u>	Total Weight (gm)
QA/QC <u>D<sup>2</sup></u>								
Date <u>9/20</u>								
Total Weight (gm)								
Impinger 2	<u>5% / 10%</u>	<u>699.3</u>	<u>518.9</u>	<u>180.4</u>				
Impinger 3	<u>5% / 10%</u>	<u>545.7</u>	<u>520.9</u>	<u>24.8</u>				
Impinger 4	<u>EMPTY</u>	<u>430.1</u>	<u>426.8</u>	<u>3.3</u>				
Impinger 5	<u>KMNO<sub>4</sub></u>	<u>529.9</u>	<u>531.8</u>	<u>-1.9</u>				
Impinger 6	<u>KMNO<sub>4</sub></u>	<u>531.7</u>	<u>531.3</u>	<u>0.4</u>				
Impinger 7	<u>GEL</u>	<u>764.0</u>	<u>739.4</u>	<u>24.6</u>	<u>581.3</u>			

Run No. <u>2</u>	Filter Type <u>QUARTZ</u>	Sample Box No. <u>71-20</u>
Date <u>9/20/05</u>	Lot No. <u>D1441301</u>	pH <u>NA</u>
Analyst <u>D<sup>2</sup></u>	Filter No. <u>NA</u>	Rinse <u>NA</u>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)				
Impinger 1	<u>EMPTY</u>	<u>830.2</u>	<u>432.5</u>	<u>397.7</u>	<table border="1" style="width: 100%; border-collapse: collapse;"> <tr> <td>QA/QC <u>D<sup>2</sup></u></td> </tr> <tr> <td>Date <u>9/20</u></td> </tr> <tr> <td>Total Weight (gm)</td> </tr> </table>	QA/QC <u>D<sup>2</sup></u>	Date <u>9/20</u>	Total Weight (gm)
QA/QC <u>D<sup>2</sup></u>								
Date <u>9/20</u>								
Total Weight (gm)								
Impinger 2	<u>5% / 10%</u>	<u>704.1</u>	<u>551.7</u>	<u>152.4</u>				
Impinger 3	<u>5% / 10%</u>	<u>578.9</u>	<u>561.7</u>	<u>17.2</u>				
Impinger 4	<u>EMPTY</u>	<u>440.6</u>	<u>438.1</u>	<u>2.5</u>				
Impinger 5	<u>KMNO<sub>4</sub></u>	<u>555.6</u>	<u>557.6</u>	<u>-2.0</u>				
Impinger 6	<u>KMNO<sub>4</sub></u>	<u>525.8</u>	<u>525.8</u>	<u>0.0</u>				
Impinger 7	<u>GEL</u>	<u>737.7</u>	<u>716.2</u>	<u>21.5</u>	<u>567.8</u> <u>589.3</u>			

Run No. <u>3</u>	Filter Type <u>QUARTZ</u>	Sample Box No. <u>67-27</u>
Date <u>9/20/05</u>	Lot No. <u>D1441301</u>	pH <u>NA</u>
Analyst <u>D<sup>2</sup></u>	Filter No. <u>NA</u>	Rinse <u>NA</u>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)				
Impinger 1	<u>EMPTY</u>	<u>778.9</u>	<u>438.2</u>	<u>340.7</u>	<table border="1" style="width: 100%; border-collapse: collapse;"> <tr> <td>QA/QC <u>D<sup>2</sup></u></td> </tr> <tr> <td>Date <u>9/21</u></td> </tr> <tr> <td>Total Weight (gm)</td> </tr> </table>	QA/QC <u>D<sup>2</sup></u>	Date <u>9/21</u>	Total Weight (gm)
QA/QC <u>D<sup>2</sup></u>								
Date <u>9/21</u>								
Total Weight (gm)								
Impinger 2	<u>5% / 10%</u>	<u>730.3</u>	<u>520.9</u>	<u>209.4</u>				
Impinger 3	<u>5% / 10%</u>	<u>529.8</u>	<u>522.1</u>	<u>7.7</u>				
Impinger 4	<u>EMPTY</u>	<u>429.4</u>	<u>428.6</u>	<u>0.8</u>				
Impinger 5	<u>KMNO<sub>4</sub></u>	<u>532.3</u>	<u>532.3</u>	<u>0.0</u>				
Impinger 6	<u>KMNO<sub>4</sub></u>	<u>532.0</u>	<u>531.6</u>	<u>.4</u>				
Impinger 7	<u>GEL</u>	<u>780.9</u>	<u>763.4</u>	<u>17.5</u>	<u>559</u> <u>576.5</u>			

# Impinger Weight Sheet

Client: <u>WHEELABRATOR</u>	Unit Name / Location: <u>3 FF OUTLET</u>
Plant: <u>NORTH</u>	Job No.: <u>9708</u> Method: <u>MA9</u>

Run No: <u>Field BLANK</u>	Filter Type: <u>QUARTZ</u>	Sample Box No: <u>67-27</u>
Date: <u>9/2/05</u>	Lot No.: <u>NA</u>	pH: <u>NA</u>
Analyst: <u>DZ</u>	Filter No.: <u>NA</u>	Rinse: <u>NA</u>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	<u>EMPTY</u>	<u>437.7</u>	<u>437.7</u>		QA/QC Date
Impinger 2	<u>5% / 10%</u>	<u>510.9</u>	<u>510.9</u>		
Impinger 3	<u>5% / 10%</u>	<u>520.8</u>	<u>520.7</u>		Total Weight (gm)
Impinger 4	<u>EMPTY</u>	<u>427.7</u>	<u>427.7</u>		
Impinger 5	<u>KMNO4</u>	<u>526.4</u>	<u>526.5</u>		
Impinger 6	<u>KMNO4</u>	<u>532.0</u>	<u>532.1</u>		
Impinger 7	<u>GEL</u>	<u>731.9</u>	<u>731.9</u>		

Run No:	Filter Type:	Sample Box No:
Date:	Lot No.:	pH:
Analyst:	Filter No.:	Rinse:

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1					QA/QC Date
Impinger 2					
Impinger 3					Total Weight (gm)
Impinger 4					
Impinger 5					
Impinger 6					
Impinger 7					

Run No:	Filter Type:	Sample Box No:
Date:	Lot No.:	pH:
Analyst:	Filter No.:	Rinse:

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1					QA/QC Date
Impinger 2					
Impinger 3					Total Weight (gm)
Impinger 4					
Impinger 5					
Impinger 6					
Impinger 7					

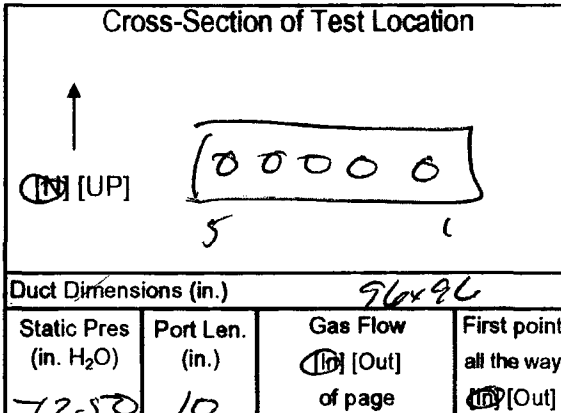
TEST LOCATION: FF Outlet  
 UNIT: 3 RUN: 4

Mercury TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 1 OF 2

Client <u>Wheelabrator</u>	Project No. <u>9704</u>
Plant <u>Alaska Railroad</u>	Date <u>9/21/05</u>
Meter Operator <u>PB</u>	
Probe Operator <u>PB</u>	

Meter Box <u>66-13</u>	Sample Box No. <u>71-20</u>
Meter Y <sub>d</sub> <u>0.98700</u>	Meter ΔH <sub>0</sub> <u>1.72905</u>
K Factor <u>3.00</u>	Pitot C <sub>p</sub> <u>0.84</u>
Leak Rate Before <u>0.004</u> [cfm] [Lpm] @ <u>15</u> (in. Hg)	
Leak Rate After <u>0.003</u> [cfm] [Lpm] @ <u>8</u> (in. Hg)	
Pitot Leak Check Before: <input checked="" type="checkbox"/> After: Good <input checked="" type="checkbox"/> Bad <input type="checkbox"/>	



Amb. Temp. (°F) <u>70</u>	Bar. Press. <u>30.50</u> (in. Hg) [mbar]
Probe I.D. No. <u>M-8-2</u>	
Liner Material <u>Coloss</u>	

Filter No. <u>N/A</u>	
Thimble No. <u>N/A</u>	
Nozzle Diameter <u>0.216</u>	Nozzle I.D. <u>2.76-1</u>

Start Time: <u>8:05</u>	Stop Time: <u>10:20</u>
-------------------------	-------------------------

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. (ft <sup>3</sup> )	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)		Filter T <sub>f</sub> (°F)		Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>min</sub> (°F)	DGM Outlet T <sub>max</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>t</sub> (°F)	Notes
						Set Points	Set Points								
	<u>5</u>			<u>21.550</u>		<u>250</u>	<u>250</u>	<u>250</u>	<u>250</u>						
1-1	5	.70	2.1	25.66	307	280	240	61	85	83	3.5	N/A			
2	10	.33	.99	28.49	298	251	250	58	87	83	2.5				
3	15	.41	1.2	31.65	303	250	257	47	90	84	3.0				
4	20	.55	1.7	35.35	306	280	241	47	91	85	3.5				
5	25	.80	2.4	39.690	307	280	253	47	93	85	4.0				
2-1	30	1.75	2.3	44.05	309	249	255	54	92	86	4.0			39.80 - 0.11	
2	35	1.70	2.1	48.13	308	280	251	51	95	87	4.0				
3	40	1.68	2.0	52.14	307	280	257	51	96	87	3.5				
4	45	1.60	1.8	55.93	307	280	243	55	96	88	3.5				
5	50	1.55	1.7	59.660	304	280	257	56	96	88	3.5				
3-1	55	1.75	2.3	63.92	308	250	253	62	93	89	4.0			57.20 - 0.04	
2	60	1.72	2.2	68.10	307	251	250	58	96	89	4.0				
									110	1024					
	Total			<u>94.075</u>											
	Average	<u>1.760</u>	<u>1.802</u>		<u>306.360</u>				<u>89.480</u>						

Sum of square roots.  
22.79

Circle correct bracketed units on data sheet.

QA/QC P<sub>2</sub>  
 Date 9/21/05

91.2400



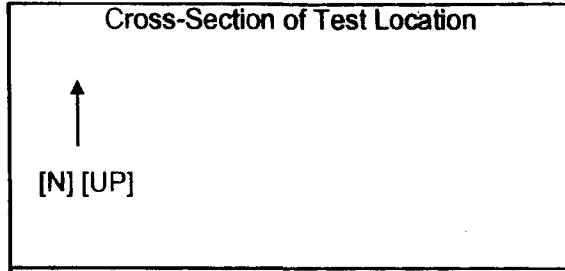
D - 12

TEST LOCATION: FF Outlet  
 UNIT: 3 RUN: 4

Mercury TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 2 OF 2

Client <u>Weyerhaeuser</u>	Project No. <u>9708</u>
Plant <u>North River</u>	Date <u>9/21/05</u>
Meter Operator <u>PB</u>	
Probe Operator <u>PB</u>	



Meter Box	Sample Box No.
Meter Y <sub>0</sub>	Meter ΔH <sub>0</sub>
K Factor	Pitot C <sub>p</sub>
Leak Rate Before [cfm] [Lpm] @ (in. Hg)	
Leak Rate After [cfm] [Lpm] @ (in. Hg)	
Pitot Leak Check Before: <input type="checkbox"/>	After: Good <input type="checkbox"/> Bad <input type="checkbox"/>

Duct Dimensions (in.)			
Static Pres (in. H <sub>2</sub> O)	Port Len. (in.)	Gas Flow [In] [Out] of page	First point all the way [In] [Out]

Amb. Temp. (°F)	Bar. Press. [in. Hg] [mbar]
Probe I.D. No.	
Liner Material	

Filter No.	
Thimble No.	
Nozzle Diameter	Nozzle I.D.

Start Time:	Stop Time:
-------------	------------

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. (L)	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)		Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>min</sub> (°F)	DGM Outlet T <sub>min</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>i</sub> (°F)	Notes
						Set Points	Set Points						
						250	250						
3	65	1.03	1.9	71.99	307	250	252	57	97	89	3.5	N/A	
4	70	1.56	1.7	75.74	305	250	246	59	97	90	3.5		
5	75	1.47	1.4	79.685	307	250	258	61	97	90	3.0		Leak check OK
4-1	80	1.20	2.1	83.29	306	250	252	63	93	90	4.0		
2	85	1.77	2.3	87.58	306	250	251	51	97	90	4.5		29.195
3	90	1.67	2.0	91.56	309	250	258	44	98	90	4.0		0.11
4	95	1.59	1.8	95.40	309	250	243	47	97	90	3.5		
5	100	1.54	1.6	99.00	306	250	254	47	97	91	3.5		99.04
5-1	105	1.8	2.4	101.10	307	249	242	55	94	90	2.5		0.049
2	110	1.68	2.0	105.05	306	250	259	58	93	90	4.0		
3	115	1.60	1.8	108.82	306	250	243	55	96	90	4.0		
4	120	1.55	1.7	112.52	307	250	251	54	96	90	3.5		
5	125	1.48	1.4	115.925	307	250	249	54	96	90	3.5		
	Total								1248	1170			
	Average												

Sum of square roots.

Circle correct bracketed units on data sheet.

QA/QC DZ  
 Date 9/21/05



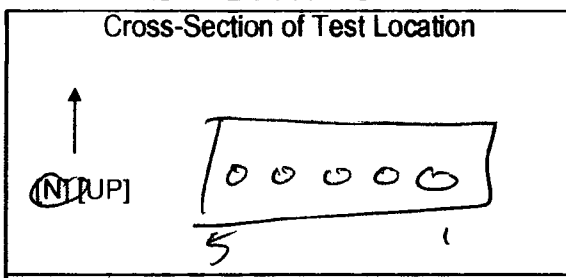
D - 13

TEST LOCATION: FF Outlet  
 UNIT: 3 RUN: 5

Mercury TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 1 OF 2

Client <u>Whirlabrator</u>	Project No. <u>9708</u>
Plant <u>North Broward</u>	Date <u>9/21/05</u>
Meter Operator <u>PB</u>	
Probe Operator <u>PB</u>	



Amb. Temp. (°F) <u>80</u>	Bar. Press. <u>30.80</u> (in. Hg) [mbar]
Probe I.D. No. <u>M-8-2</u>	
Liner Material <u>glass</u>	

Meter Box <u>66-13</u>	Sample Box No. <u>67-27</u>
Meter Y <sub>d</sub> <u>0.98700</u>	Meter ΔH <sub>0</sub> <u>1.790</u>
K Factor <u>3.00</u>	Pitot C <sub>p</sub> <u>0.44</u>
Leak Rate Before <u>0.004</u> (Lpm) @ <u>15</u> (in. Hg)	
Leak Rate After <u>0.004</u> (Lpm) @ <u>8</u> (in. Hg)	
Pitot Leak Check Before: <input checked="" type="checkbox"/> After: Good <input type="checkbox"/> Bad <input type="checkbox"/>	

Duct Dimensions (in.) <u>96 x 96</u>			
Static Pres (in. H <sub>2</sub> O) <u>-12.50</u>	Port Len. (in.) <u>10</u>	Gas Flow (in) [Out] of page <u>(in) [Out]</u>	First point all the way <u>(in) [Out]</u>

Filter No. <u>N/A</u>	
Thimble No. <u>N/A</u>	
Nozzle Diameter <u>0.276</u>	Nozzle I.D. <u>2.761</u>

Start Time: <u>10:43</u>	Stop Time: <u>12:59</u>
--------------------------	-------------------------

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. (in) [L]	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)	Filter T <sub>f</sub> (°F)	Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>m in</sub> (°F)	DGM Outlet T <sub>m out</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>t</sub> (°F)	Notes
						Set Points							
1-1	5	.35	1.0	116.195	298	248	250	43	90	89	2.5	N/A	
2	10	.37	1.1	122.4	298	250	254	48	91	89	2.5		
3	15	.37	1.1	125.01	303	250	246	43	93	89	2.5		
4	20	.45	1.4	128.39	306	280	252	42	93	89	3.0		
5	25	.53	1.6	132.01	306	250	255	43	94	89	3.0		
2-1	30	.62	1.9	135.136.04	307	250	242	49	93	90	3.5		132.135 -0.125
2	35	.48	1.4	139.43	306	250	243	45	96	90	3.0		
3	40	.53	1.6	143.04	306	250	242	46	98	91	3.5		
4	45	.60	1.8	146.85	307	250	257	47	99	91	3.5		
5	56	.57	1.7	150.535	308	250	242	48	99	91	3.5		
3-1	55	.36	1.1	153.55	307	249	259	54	95	92	3.0		150.565
2	60	.53	1.6	157.18	307	250	245	51	96	92	3.5		-0.03
Total				86.0125									
Average		0.647	1.464	305.720					93.9600				

\* Sum of square roots.

Circle correct bracketed units on data sheet.

12.3

85.9000

2219 QA/QC: DZ  
 Date: 9/21/05

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TEST LOCATION: FF Outlet  
 UNIT: 3 RUN: 5

Mercury TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 2 OF 2

Client <u>Wheelabrator</u>	Project No. <u>9708</u>
Plant <u>North Branch</u>	Date <u>9/21/05</u>
Meter Operator <u>PB</u>	
Probe Operator <u>PB</u>	

Meter Box	Sample Box No.
Meter Y <sub>d</sub>	Meter ΔH <sub>@</sub>
K Factor	Pitot C <sub>p</sub>
Leak Rate Before [cfm] [Lpm] @ (in. Hg)	
Leak Rate After [cfm] [Lpm] @ (in. Hg)	
Pitot Leak Check Before: <input type="checkbox"/>	After: Good <input type="checkbox"/> Bad <input type="checkbox"/>

Cross-Section of Test Location

↑  
[N] [UP]

Duct Dimensions (in.)			
Static Pres (in. H <sub>2</sub> O)	Port Len. (in.)	Gas Flow [In] [Out] of page	First point all the way [In] [Out]

Amb. Temp. (°F)	Bar. Press. [in. Hg] [mbar]
Probe I.D. No.	
Liner Material	

Filter No.	
Thimble No.	
Nozzle Diameter	Nozzle I.D.

Start Time:	Stop Time:
-------------	------------

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. (L)	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)	Filter T <sub>f</sub> (°F)	Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>m in</sub> (°F)	DGM Outlet T <sub>m out</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>t</sub> (°F)	Notes
						Set Points							
3	65	153	1.6	160.80	307	250	259	50	98	92	3.5	N/A	
4	70	150	1.5	164.29	308	250	248	51	98	93	3.5		
5	75	145	1.4	167.660	307	256	259	53	98	93	3.5		
4-1	80	160	1.8	171.55	307	250	244	57	95	92	3.5		167.765
2	85	155	1.7	175.24	307	250	251	46	98	92	3.5		Leak U/O K
3	90	150	1.5	178.72	305	250	244	43	97	92	3.5		-0.105
4	95	147	1.4	182.08	307	250	257	43	97	92	3.5		
5	100	147	1.4	185.445	308	250	241	44	98	93	3.5		185.585
5-1	105	142	1.3	188.77	305	249	259	50	96	93	3.0		-0.06
2	110	143	1.3	192.02	304	250	252	46	99	93	3.0		
3	115	148	1.4	195.42	305	250	250	47	100	94	3.5		
4	120	155	1.7	199.14	307	250	249	47	99	94	4.0		
5	125	143	1.3	202.465	307	250	253	47	99	94	3.0		
	Total												
	Average												

\*Sum of square roots.

Circle correct bracketed units on data sheet.

QA/QC DJ  
 Date 9/21/05



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TEST LOCATION: PP Outlet  
 UNIT: 3 RUN: 60

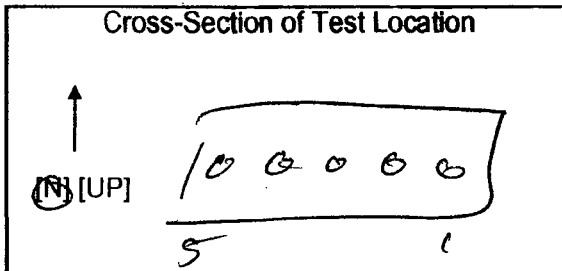
Mercury TESTING  
**FIELD DATA SHEET**

METHOD: 29 PAGE 1 OF 2

Client <u>Wick Laboratories</u>	Project No. <u>9708</u>
Plant <u>North Broward</u>	Date <u>9/21/05</u>
Meter Operator <u>PB</u>	
Probe Operator <u>PB</u>	

Meter Box <u>66-13</u>	Sample Box No. <u>71-20</u>
Meter Yd <u>0.98700</u>	Meter ΔH <sub>0</sub> <u>1.7408</u>
K Factor <u>3.00</u>	Pitot Cp <u>0.84</u>

Leak Rate Before <u>0.005</u> [cfm] [Lpm] @ <u>15</u> (in. Hg)
Leak Rate After <u>0.005</u> [cfm] [Lpm] @ <u>9</u> (in. Hg)
Pitot Leak Check Before: <input checked="" type="checkbox"/> After: Good <input checked="" type="checkbox"/> Bad <input type="checkbox"/>



Duct Dimensions (in.) <u>9.6 x 9.6</u>			
Static Pres (in. H <sub>2</sub> O) <u>-12.30</u>	Port Len. (in.) <u>10</u>	Gas Flow (ft <sup>3</sup> /min) [Out] <u>10</u>	First point all the way (ft) [Out] <u>10</u>

Amb. Temp. (°F) <u>70</u>	Bar. Press. <u>30.52</u> (in. Hg) [mbar]
Probe I.D. No. <u>M-8-2</u>	
Liner Material <u>Glass</u>	

Filter No. <u>N/A</u>	
Thimble No. <u>N/A</u>	
Nozzle Diameter <u>0.270</u>	Nozzle I.D. <u>270-1</u>

Start Time: <u>13:15</u>	Stop Time: <u>15:29</u>
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Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. (ft <sup>3</sup> ) [L]	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)		Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>min</sub> (°F)	DGM Outlet T <sub>out</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>i</sub> (°F)	Notes
						Set Points	Set Points						
1-1	5	.28	.84	202.670	291.0	248	250	64	95	94	2.5	N/A	
2	10	.30	.90	207.97	291.0	250	244	63	96	94	2.5		
3	15	.41	1.2	211.13	304	249	239	56	95	94	3.0		
4	20	.50	1.5	214.60	308	250	245	54	97	94	3.0		
5	25	.62	1.9	218.510	308	250	240	55	98	94	3.5		218.510
2-1	30	.75	2.3	222.85	309	250	243	57	97	94	4.0		(-0.05)
2	35	.62	1.9	226.79	308	249	240	58	99	94	3.5		
3	40	.53	1.6	230.42	305	250	247	59	100	95	3.0		
4	45	.45	1.4	233.79	307	250	240	62	100	95	3.0		
5	50	.48	1.4	237.165	307	250	240	58	101	95	3.0		237.220
3-1	55	.47	1.4	240.61	306	250	247	60	98	96	3.0		(-0.05)
2	60	.51	1.5	244.13	305	250	241	58	101	96	3.5		
Total				1.4956									
Average				0.1957									

Sum of square roots. 17.84

Circle correct bracketed units on data sheet. 307.880

97.3200  
2300

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TEST LOCATION: EF Outlet  
 UNIT: 3 RUN: 6

Mercury TESTING  
**FIELD DATA SHEET**

METHOD: 24 PAGE 2 OF 2

Client <u>Wheelabrator</u>	Project No. <u>9708</u>
Plant <u>Waste Brewer</u>	Date <u>9/2/05</u>
Meter Operator <u>PB</u>	
Probe Operator <u>PB</u>	

Meter Box	Sample Box No.
Meter Y <sub>d</sub>	Meter ΔH <sub>@</sub>
K Factor	Pitot C <sub>p</sub>
Leak Rate Before [cfm] [Lpm] @ (in. Hg)	
Leak Rate After [cfm] [Lpm] @ (in. Hg)	
Pitot Leak Check Before: <input type="checkbox"/> After: Good <input type="checkbox"/> Bad <input type="checkbox"/>	

Cross-Section of Test Location

↑  
[N] [UP]

Duct Dimensions (in.)

Static Pres (in. H <sub>2</sub> O)	Port Len. (in.)	Gas Flow [In] [Out] of page	First point all the way [In] [Out]
------------------------------------	-----------------	-----------------------------	------------------------------------

Amb. Temp. (°F)	Bar. Press. [in. Hg] [mbar]
Probe I.D. No.	
Liner Material	

Filter No.	
Thimble No.	
Nozzle Diameter	Nozzle I.D.

Start Time: \_\_\_\_\_ Stop Time: \_\_\_\_\_

Traverse Point Number	Min/pt Elapsed Time	Velocity Head ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume V <sub>m</sub> Init. Vol. [L]	Stack Temp. T <sub>s</sub> (°F)	Probe T <sub>p</sub> (°F)	Filter T <sub>f</sub> (°F)	Cond. Temp. T <sub>c</sub> (°F)	DGM Inlet T <sub>m in</sub> (°F)	DGM Outlet T <sub>m out</sub> (°F)	Pump Vacuum (in. Hg)	XAD Trap Temp. T <sub>t</sub> (°F)	Notes
						Set Points							
3	65	.53	1.6	247.76	304	250	241	58	102	97	3.5	N/A	
4	70	.47	1.4	251.16	307	250	247	61	102	97	3.0		valve OK
5	75	.42	1.3	254.420	308	250	242	64	101	97	3.0		<del>254.525</del>
4-1	80	.63	1.9	258.43	307	250	248	64	99	97	4.0		(-0.105)
2	85	.65	2.0	262.45	307	250	249	58	102	97	4.0		
3	90	.55	1.7	266.18	306	250	240	51	103	97	3.5		
4	95	.53	1.6	269.81	309	250	243	51	103	97	3.5		
5	100	.45	1.4	273.245	310	250	247	53	103	97	3.5		
5-1	105	.15	.45	275.110	310	250	249	62	96	96	2.5		273.285
2	110	.55	1.7	278.86	312	250	250	61	96	96	4.0		(0.04)
3	115	.55	1.7	282.57	315	250	249	56	98	95	4.0		
4	120	.48	1.4	285.94	325	249	247	57	98	95	3.5		
5	125	.45	1.4	289.300	316	250	251	57	98	95	3.5		
	Total												
	Average												

Sum of square roots. Circle correct bracketed units on data sheet.

QA/QC \_\_\_\_\_  
 Date \_\_\_\_\_



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# ORSAT READINGS

TEST LOCATION: FF OUTLET-3

PAGE 1 OF 1

Client:	WHEELABRATOR	Project Number:	9708	$F_o = \frac{20.9 - \%O_2}{\%CO_2}$
Plant:	NORTH	Unit:	3	
Orsat ID:	3	Fuel Type:	mw	Leak Check Passed <input checked="" type="checkbox"/>

Run Number	Method Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Fo	Analyst	Analysis	
								Date	Time
4	m29	1	9.2	19.4	10.2		D <sup>3</sup>	9/21	1136
		2	9.2	19.4	10.2				
		3	9.2	19.4	10.2				
		Avg:	9.2		10.2				
5	m29	1	9.2	19.2	10.0		D <sup>3</sup>	9/21	1406
		2	9.2	19.2	10.0				
		3	9.2	19.2	10.0				
		Avg:	9.2		10.0				
6	m29	1	9.2	19.4	10.2		D <sup>3</sup>	9/21	1549
		2	9.2	19.4	10.2				
		3	9.2	19.4	10.2				
		Avg:	9.2		10.2				
		1							
		2							
		3							
		Avg:							
		1							
		2							
		3							
		Avg:							
		1							
		2							
		3							
		Avg:							

Repeat the analysis procedure until the results of any three analyses differ by no more than 0.2 percent by volume. Average the three acceptable values and report the results to the nearest 0.1 percent. Calculate Fo to verify result.

Acceptable ranges for Fo:

Coal:	Anthracite and lignite	1.016-1.130	Gas:	Natural	1.600-1.836
	Bituminous	1.083-1.230		Propane	1.434-1.586
Oil:	Distillate	1.260-1.413		Butane	1.405-1.553
	Residual	1.210-1.370	Wood:		1.000-1.120

# Impinger Weight Sheet

Client <b>WHEELABRATOR</b>	Unit Name / Location <b>3 FF OUTLET</b>
Plant <b>NORTH</b>	Job No: <b>9708</b> Method: <b>ma9</b>

Run No: <b>4</b>	Filter Type <b>QUARTZ</b>	Sample Box No: <b>71-20</b>
Date: <b>9/21/05</b>	Lot No: <b>D1441301</b>	pH: <b>NA</b>
Analyst: <b>D<sup>2</sup></b>	Filter No: <b>NA</b>	Rinse: <b>NA</b>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	EMPTY	794.0	434.2	359.8	
Impinger 2	5% / 10%	667.1	552.5	114.6	QA/QC <b>5/4</b> Date <b>D<sup>2</sup></b>
Impinger 3	5% / 10%	589.3	571.6	17.7	
Impinger 4	EMPTY	441.3	439.5	1.8	
Impinger 5	KMNO <sub>4</sub>	529.9	529.7	0.2	Total Weight (gm)
Impinger 6	KMNO <sub>4</sub>	559.0	559.6	-0.6	<b>493.5</b>
Impinger 7	GEL	770.6	749.6	21.0	<b>514.5</b>

Run No: <b>5</b>	Filter Type <b>QUARTZ</b>	Sample Box No: <b>62-27</b>
Date: <b>9/21/05</b>	Lot No: <b>D1441301</b>	pH: <b>NA</b>
Analyst: <b>D<sup>2</sup></b>	Filter No: <b>NA</b>	Rinse: <b>NA</b>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	EMPTY	806.4	437.9	368.5	
Impinger 2	5% / 10%	597.4	511.9	85.5	QA/QC <b>D<sup>3</sup></b> Date <b>5/4</b>
Impinger 3	5% / 10%	526.6	521.5	5.1	
Impinger 4	EMPTY	428.6	427.9	0.7	
Impinger 5	KMNO <sub>4</sub>	528.4	527.4	1.0	Total Weight (gm)
Impinger 6	KMNO <sub>4</sub>	533.6	533.0	0.6	<b>461.4</b>
Impinger 7	GEL	748.5	731.9	16.6	<b>478</b>

Run No: <b>6</b>	Filter Type <b>QUARTZ</b>	Sample Box No: <b>71-20</b>
Date: <b>9/21/05</b>	Lot No: <b>D1441301</b>	pH: <b>NA</b>
Analyst: <b>D<sup>2</sup></b>	Filter No: <b>NA</b>	Rinse: <b>NA</b>

	Contents	Gross Weight (gm)	Tare Weight (gm)	Net Weight Gain (gm)	
Impinger 1	EMPTY	797.0	433.9	363.1	
Impinger 2	5% / 10%	641.7	548.4	93.3	QA/QC <b>D<sup>3</sup></b> Date <b>9/22</b>
Impinger 3	5% / 10%	582.9	571.1	11.8	
Impinger 4	EMPTY	442.2	439.8	2.4	
Impinger 5	KMNO <sub>4</sub>	561.8	561.8	0.0	Total Weight (gm)
Impinger 6	KMNO <sub>4</sub>	532.2	531.7	0.5	<b>471.1</b>
Impinger 7	GEL	786.7	769.8	16.9	<b>488.0</b>

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WHEELABRATOR NORTH BROWARD  
POMPANO BEACH, FLORIDA

Client Reference No: 14500124  
CleanAir Project No: 9708-4

**FIELD DATA PRINTOUTS**

E

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Field Data Printout

Test Method: USEPA Method 29  
 Analyte: Mercury

Location: Unit 3 FF Outlet  
 Test Run: 1  
 Client: Wheelabrator North Broward, Inc  
 Project No: 9708  
 Source Area (ft<sup>2</sup>): 64.00000

Bar. Press. (in. Hg): 30.00  
 Static P: -11.1  
 O<sub>2</sub> (dry volume %): 9.40  
 CO<sub>2</sub> (dry volume %): 9.60  
 N<sub>2</sub>+CO (dry volume %): 81.00

Nozzle ID No: 276-1  
 Nozzle Diameter (D<sub>n</sub>): 0.276  
 Probe ID No: M-8-2  
 Pitot C<sub>p</sub>: 0.84  
 Pitot Leak Check:  Pass  Fail

Test Date: 9/20/05  
 Start Time: 08:30  
 Stop Time: 11:18  
 Leak Rate Before: 0.007 cfm @ 15 "Hg  
 Leak Rate After: 0.005 cfm @ 9 "Hg

H<sub>2</sub>O (condensate, ml or gm): 556.7  
 H<sub>2</sub>O (silica, g): 24.6  
 Actual Moisture (%): 24.15

Meter Box ID No: 66-13  
 Meter ΔH@: 1.79910  
 Meter Y<sub>0</sub>: 0.98700

Traverse Point	Run Time 5.0 min/read	Pitot ΔP <sub>s</sub> (in. H <sub>2</sub> O)	Sample ΔH (in. H <sub>2</sub> O)	Metered (dcf)	Stack T <sub>s</sub> (°F)	Dry Gas Meter		√ΔP <sub>s</sub> (calculated) (√in. H <sub>2</sub> O)	Volume (calculated) (ft <sup>3</sup> )	Isokinetics (calculated) (%)
						T <sub>m-in</sub> (°F)	T <sub>m-out</sub> (°F)			
	0.0			755.410						
1-01	5.0	0.28	0.84	757.950	295	82	81	0.53	2.54	102.5
1-02	10.0	0.38	1.10	760.900	301	82	81	0.62	2.95	102.6
1-03	15.0	0.50	1.50	764.320	307	85	81	0.71	3.42	104.0
1-04	20.0	0.51	1.50	767.750	307	89	82	0.71	3.43	102.8
1-05	25.0	0.56	1.70	771.395	307	91	83	0.75	3.64	104.0
Leak-Check	25.0			771.510						
2-01	30.0	0.86	2.60	775.950	309	93	85	0.93	4.44	102.2
2-02	35.0	0.68	2.00	779.920	309	95	85	0.82	3.97	102.4
2-03	40.0	0.63	1.90	783.750	307	97	87	0.79	3.83	102.1
2-04	45.0	0.58	1.70	787.420	307	97	87	0.76	3.67	101.9
2-05	50.0	0.63	1.90	791.300	309	97	88	0.79	3.88	103.5
Leak-Check	50.0			791.382						
3-01	55.0	0.58	1.70	795.020	309	96	89	0.76	3.64	101.1
3-02	60.0	0.74	2.20	799.130	308	97	89	0.86	4.11	101.1
3-03	65.0	0.67	2.00	803.150	309	99	90	0.82	4.02	103.6
3-04	70.0	0.61	1.80	806.930	309	99	90	0.78	3.78	102.1
3-05	75.0	0.43	1.30	810.200	299	93	90	0.66	3.27	104.9
Leak-Check	75.0			810.320						
4-01	80.0	0.63	1.90	814.190	299	96	91	0.79	3.87	102.4
4-02	85.0	0.65	2.00	818.150	300	98	91	0.81	3.96	103.0
4-03	90.0	0.58	1.70	821.870	299	100	92	0.76	3.72	102.0
4-04	95.0	0.50	1.50	825.320	296	101	93	0.71	3.45	101.5
4-05	100.0	0.43	1.30	828.590	299	101	93	0.66	3.27	103.9
Leak-Check	100.0			828.640						
5-01	105.0	0.51	1.50	832.070	297	99	93	0.71	3.43	100.2
5-02	110.0	0.55	1.70	835.800	299	101	94	0.74	3.73	104.8
5-03	115.0	0.54	1.60	839.400	299	101	94	0.73	3.60	102.0
5-04	120.0	0.51	1.50	842.860	297	102	94	0.71	3.46	100.7
5-05	125.0	0.45	1.40	846.240	299	102	94	0.67	3.38	104.8
Final	125.0		1.67360	90.46300	303.04000	92.20000		0.74373	90.46300	

25 points sampled

QC-Check: Field Averages	0.7437	1.6736	90.4630	303.0400	92.2000
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Avg. OK     Avg. OK     Avg. OK     Avg. OK     Avg. OK

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Field Data Printout

Test Method: USEPA Method 29  
 Analyte: Mercury

Location: Unit 3 FF Outlet  
 Test Run: 2  
 Client: Wheelabrator North Broward, Inc  
 Project No: 9708  
 Source Area (ft<sup>2</sup>): 64.00000

Bar. Press. (in. Hg): 30.00  
 Static P.: -11.0

Nozzle ID No: 276-1  
 Nozzle Diameter (D<sub>n</sub>): 0.276  
 Probe ID No: M-8-2  
 Pitot C<sub>p</sub>: 0.84

Test Date: 9/20/05  
 Start Time: 12:04  
 Stop Time: 14:17  
 Leak Rate Before: 0.006 cfm  
 Leak Rate After: 0.003 cfm

O<sub>2</sub> (dry volume %): 9.40  
 CO<sub>2</sub> (dry volume %): 9.80  
 N<sub>2</sub>+CO (dry volume %): 80.80

Pitot Leak Check:  Pass  Fail

H<sub>2</sub>O (condensate, ml or gm): 567.8  
 H<sub>2</sub>O (silica, g): 21.5  
 Actual Moisture (%): 25.07

Meter Box ID No: 66-13  
 Meter ΔH@: 1.79910  
 Meter Y<sub>0</sub>: 0.98700

Traverse Point	Run Time 5.0 min/read	Pitot ΔP <sub>s</sub> (in. H <sub>2</sub> O)	Sample ΔH (in. H <sub>2</sub> O)	Metered (dcf)	Stack T <sub>s</sub> (°F)	Dry Gas Meter		√ΔP <sub>s</sub> (calculated) (√in. H <sub>2</sub> O)	Volume (calculated) (ft <sup>3</sup> )	Isokinetics (calculated) (%)
						T <sub>m-in</sub> (°F)	T <sub>m-out</sub> (°F)			
	0.0			847.045						
1-01	5.0	0.55	1.70	850.760	295	83	85	0.74	3.72	107.8
1-02	10.0	0.53	1.60	854.332	292	85	85	0.73	3.57	105.2
1-03	15.0	0.40	1.20	857.460	291	87	84	0.63	3.13	105.7
1-04	20.0	0.53	1.60	861.070	297	88	84	0.73	3.61	106.4
1-05	25.0	0.56	1.70	864.775	297	89	84	0.75	3.70	106.2
Leak-Check	25.0			864.810						
2-01	30.0	0.68	2.00	868.740	298	88	83	0.82	3.93	102.6
2-02	35.0	0.53	1.60	872.330	297	90	83	0.73	3.59	105.7
2-03	40.0	0.48	1.40	875.680	297	90	83	0.69	3.35	103.6
2-04	45.0	0.47	1.40	879.040	298	90	84	0.69	3.36	105.0
2-05	50.0	0.42	1.30	882.270	297	90	84	0.65	3.23	106.7
Leak-Check	50.0			882.305						
3-01	55.0	0.57	1.70	885.970	297	88	84	0.75	3.67	104.2
3-02	60.0	0.61	1.80	889.750	297	90	84	0.78	3.78	103.7
3-03	65.0	0.57	1.70	893.420	295	91	84	0.75	3.67	103.9
3-04	70.0	0.50	1.50	896.910	299	92	84	0.71	3.49	105.7
3-05	75.0	0.43	1.30	900.140	298	92	84	0.66	3.23	105.3
Leak-Check	75.0			900.250						
4-01	80.0	0.58	1.70	903.890	296	89	85	0.76	3.64	102.4
4-02	85.0	0.59	1.80	907.710	297	92	85	0.77	3.82	106.3
4-03	90.0	0.51	1.50	911.170	297	93	85	0.71	3.46	103.4
4-04	95.0	0.47	1.40	914.510	297	94	86	0.69	3.34	103.8
4-05	100.0	0.38	1.10	917.460	297	94	86	0.62	2.95	101.8
Leak-Check	100.0			917.515						
5-01	105.0	0.42	1.30	920.730	296	91	86	0.65	3.22	105.8
5-02	110.0	0.44	1.30	923.950	297	93	87	0.66	3.22	103.4
5-03	115.0	0.45	1.40	927.320	297	95	88	0.67	3.37	106.7
5-04	120.0	0.45	1.40	930.660	296	95	88	0.67	3.34	105.7
5-05	125.0	0.42	1.30	933.905	297	95	88	0.65	3.25	106.3
Final	125.0									
25 points sampled		Sq. RLAP								
QC-Check: Field Averages		0.7063	1.5060	86.6250	296.4800	87.7400		0.70633	86.62500	

Avg. OK  Avg. OK  Avg. OK  Avg. OK  Avg. OK

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Field Data Printout

Test Method: USEPA Method 29  
 Analyte: Mercury

Location: Unit 3 FF Outlet  
 Test Run: 3  
 Client: Wheelabrator North Broward, Inc  
 Project No: 9708  
 Source Area (ft<sup>2</sup>): 64.00000

Bar. Press. (in. Hg): 30.00  
 Static P.: 30.0  
 O<sub>2</sub> (dry volume %): 9.60  
 CO<sub>2</sub> (dry volume %): 9.40  
 N<sub>2</sub>+CO (dry volume %): 81.00

Nozzle ID No: 276-1  
 Nozzle Diameter (D<sub>n</sub>): 0.276  
 Probe ID No: M-B-2  
 Pitot C<sub>p</sub>: 0.84  
 Pitot Leak Check:  Pass  Fail

Test Date: 9/20/05  
 Start Time: 14:35  
 Stop Time: 16:50  
 Leak Rate Before: 0.004 cfm  
 Leak Rate After: 0.003 cfm

@ 15 "Hg  
 @ 8 "Hg

H<sub>2</sub>O (condensate, ml or gm): 559.0  
 H<sub>2</sub>O (silica, g): 17.5  
 Actual Moisture (%): 24.87

Meter Box ID No: 66-13  
 Meter ΔH @: 1.79910  
 Meter Y<sub>d</sub>: 0.98700

Traverse Point	Run Time 5.0 min/read	Pitot ΔP <sub>s</sub> (in. H <sub>2</sub> O)	Sample ΔH (in. H <sub>2</sub> O)	Metered (dof)	Stack T <sub>s</sub> (°F)	Dry Gas Meter		√ΔP <sub>s</sub> (calculated) (√in. H <sub>2</sub> O)	Volume (calculated) (ft <sup>3</sup> )	Isokinetics (calculated) (%)
						T <sub>m-in</sub> (°F)	T <sub>m-out</sub> (°F)			
	0.0			934.180						
1-01	5.0	0.23	0.69	936.550	283	88	88	0.48	2.37	99.2
1-02	10.0	0.25	0.75	939.010	284	90	88	0.50	2.46	98.6
1-03	15.0	0.32	0.96	941.770	295	91	88	0.57	2.76	98.5
1-04	20.0	0.41	1.20	944.890	296	92	88	0.64	3.12	98.4
1-05	25.0	0.58	1.70	948.555	298	94	89	0.76	3.66	97.2
Leak-Check	25.0			948.620						
2-01	30.0	0.73	2.20	952.710	297	94	89	0.85	4.09	96.7
2-02	35.0	0.66	2.00	956.680	300	96	89	0.81	3.97	98.7
2-03	40.0	0.57	1.70	960.410	298	97	90	0.75	3.73	99.4
2-04	45.0	0.51	1.50	963.910	296	97	90	0.71	3.50	98.4
2-05	50.0	0.47	1.40	967.260	297	96	90	0.69	3.35	98.2
Leak-Check	50.0			967.295						
3-01	55.0	0.53	1.60	970.860	297	94	90	0.73	3.57	98.7
3-02	60.0	0.64	1.80	974.750	298	96	91	0.80	3.89	97.9
3-03	65.0	0.58	1.70	978.460	302	97	91	0.76	3.71	98.2
3-04	70.0	0.50	1.50	981.970	301	97	91	0.71	3.51	99.9
3-05	75.0	0.45	1.40	985.325	297	97	91	0.67	3.36	100.4
Leak-Check	75.0			985.425						
4-01	80.0	0.62	1.90	989.310	296	93	91	0.79	3.88	99.4
4-02	85.0	0.62	1.90	993.190	297	97	91	0.79	3.88	99.0
4-03	90.0	0.53	1.60	996.800	298	97	91	0.73	3.61	99.6
4-04	95.0	0.53	1.60	1000.410	298	97	91	0.73	3.61	99.6
4-05	100.0	0.45	1.40	1003.830	297	97	91	0.67	3.42	102.3
Leak-Check	100.0			1003.890						
5-01	105.0	0.48	1.40	1007.270	298	94	91	0.69	3.38	98.2
5-02	110.0	0.53	1.60	1010.860	299	96	91	0.73	3.59	99.2
5-03	115.0	0.53	1.60	1014.430	298	98	91	0.73	3.57	98.4
5-04	120.0	0.48	1.40	1017.850	297	98	91	0.69	3.42	99.0
5-05	125.0	0.38	1.10	1020.870	297	98	91	0.62	3.02	98.2
Final	125.0		1.50800	86.43000	296.56000	92.68000		0.70384	86.43000	

25 points sampled

QC-Check: Field Averages	0.7038	1.5080	86.4300	296.5600	92.6800
	<input checked="" type="checkbox"/> Avg. OK	<input checked="" type="checkbox"/> Avg. OK	<input checked="" type="checkbox"/> Avg. OK	<input checked="" type="checkbox"/> Avg. OK	<input checked="" type="checkbox"/> Avg. OK

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USEPA Method 4 Laboratory Data

Location: Unit 3 FF Outlet  
 Client: Wheelabrator North Broward, Inc  
 Project No: 9708

Test Method: USEPA Method 29  
 Analyte: Mercury

Test Run:

Contents	Gross (gm)	Tare (gm)	Net (gm)		Field Data Check
Impinger 1 Empty	786.5	436.8	349.7		
Impinger 2 5%HNO3/10%H2O2	699.3	518.9	180.4		
Impinger 3 5%HNO3/10%H2O2	545.7	520.9	24.8		
Impinger 4 Empty	430.1	426.8	3.3		
Impinger 5 4%KMnO4/10%H2SO4	529.9	531.8	-1.9		
Impinger 6 4%KMnO4/10%H2SO4	531.7	531.3	0.4	556.7 Liquid (gm)	
Impinger 7 Silica Gel	764.0	739.4	24.6	0.0 less rinse (gm)	
Impinger 8				556.7 Net Liquid (gm)	<input type="checkbox"/> QA/QC OK
				+ 24.6 Silica Gel (gm)	<input type="checkbox"/> QA/QC OK
				581.3 Total Vlc (gm)	<input type="checkbox"/> QA/QC OK

Rinse:  (ml or gm)

Test Run:

Contents	Gross (gm)	Tare (gm)	Net (gm)		Field Data Check
Impinger 1 Empty	830.2	432.5	397.7		
Impinger 2 5%HNO3/10%H2O2	704.1	551.7	152.4		
Impinger 3 5%HNO3/10%H2O2	578.9	561.7	17.2		
Impinger 4 Empty	440.6	438.1	2.5		
Impinger 5 4%KMnO4/10%H2SO4	555.6	557.6	-2.0		
Impinger 6 4%KMnO4/10%H2SO4	525.8	525.8	0.0	567.8 Liquid (gm)	
Impinger 7 Silica Gel	737.7	716.2	21.5	0.0 less rinse (gm)	
Impinger 8				567.8 Net Liquid (gm)	<input type="checkbox"/> QA/QC OK
				+ 21.5 Silica Gel (gm)	<input type="checkbox"/> QA/QC OK
				589.3 Total Vlc (gm)	<input type="checkbox"/> QA/QC OK

Rinse:  (ml or gm)

Test Run:

Contents	Gross (gm)	Tare (gm)	Net (gm)		Field Data Check
Impinger 1 Empty	778.9	438.2	340.7		
Impinger 2 5%HNO3/10%H2O2	730.3	520.9	209.4		
Impinger 3 5%HNO3/10%H2O2	529.8	522.1	7.7		
Impinger 4 Empty	429.4	426.6	0.8		
Impinger 5 4%KMnO4/10%H2SO4	532.3	532.3	0.0		
Impinger 6 4%KMnO4/10%H2SO4	532.0	531.6	0.4	559.0 Liquid (gm)	
Impinger 7 Silica Gel	780.9	763.4	17.5	0.0 less rinse (gm)	
Impinger 8				559.0 Net Liquid (gm)	<input type="checkbox"/> QA/QC OK
				+ 17.5 Silica Gel (gm)	<input type="checkbox"/> QA/QC OK
				576.5 Total Vlc (gm)	<input type="checkbox"/> QA/QC OK

Rinse:  (ml or gm)

Test Run:

Contents	Gross (gm)	Tare (gm)	Net (gm)		Field Data Check
Impinger 1 Empty					
Impinger 2 5%HNO3/10%H2O2					
Impinger 3 5%HNO3/10%H2O2					
Impinger 4 Empty					
Impinger 5 4%KMnO4/10%H2SO4					
Impinger 6 4%KMnO4/10%H2SO4				Liquid (gm)	
Impinger 7 Silica Gel				less rinse (gm)	
Impinger 8				Net Liquid (gm)	<input type="checkbox"/> QA/QC OK
				Silica Gel (gm)	<input type="checkbox"/> QA/QC OK
				Total Vlc (gm)	<input type="checkbox"/> QA/QC OK

Rinse:  (ml or gm)

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USEPA Method 3 Laboratory Data

Location: Unit 3 FF Outlet  
 Client: Wheelabrator North Broward, Inc  
 Project No: 9708  
 Method: EPA Method 3  
 Fuel Type: Municipal Waste  
 F<sub>o</sub> for Fuel: 1.03 to 1.3

Test Method: USEPA Method 29  
 Analyte: Mercury

Run Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Percent N <sub>2</sub>	Dry Mol. Weight	F <sub>o</sub>	Method of Analysis: Orsat
1	1	9.6	19.0	9.4	81.0	29.91	1.19792	All measurements in spec.
	2	9.6	19.0	9.4	81.0	29.91		
	3	9.6	19.0	9.4	81.0	29.91		
Avg.		9.60000		9.40000	81.00000	29.91		
CEM or Other Avg:		9.60000		9.40000	81.00000	29.91200		<input checked="" type="checkbox"/> F <sub>o</sub> value within expected range.

Run Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Percent N <sub>2</sub>	Dry Mol. Weight	F <sub>o</sub>	Method of Analysis: Orsat
2	1	9.8	19.2	9.4	80.8	29.94	1.17347	All measurements in spec.
	2	9.8	19.2	9.4	80.8	29.94		
	3	9.8	19.2	9.4	80.8	29.94		
Avg.		9.80000		9.40000	80.80000	29.94		
CEM or Other Avg:		9.80000		9.40000	80.80000	29.94400		<input checked="" type="checkbox"/> F <sub>o</sub> value within expected range.

Run Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Percent N <sub>2</sub>	Dry Mol. Weight	F <sub>o</sub>	Method of Analysis: Orsat
3	1	9.4	19.0	9.6	81.0	29.89	1.20213	All measurements in spec.
	2	9.4	19.0	9.6	81.0	29.89		
	3	9.4	19.0	9.6	81.0	29.89		
Avg.		9.40000		9.60000	81.00000	29.89		
CEM or Other Avg:		9.40000		9.60000	81.00000	29.88800		<input checked="" type="checkbox"/> F <sub>o</sub> value within expected range.

Run Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Percent N <sub>2</sub>	Dry Mol. Weight	F <sub>o</sub>	Method of Analysis: Orsat
	1							
	2							
	3							
Avg.								
CEM or Other Avg:								<input type="checkbox"/> F <sub>o</sub> value within expected range.

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Field Data Printout

Test Method: USEPA Method 29  
 Analyte: Mercury

Location: Unit 3 FF Outlet  
 Test Run: 4  
 Client: Wheelabrator North Broward, Inc  
 Project No: 9708  
 Source Area (ft<sup>2</sup>): 64.00000

Bar. Press. (in. Hg): 30.50  
 Static P: -12.5  
 O<sub>2</sub> (dry volume %): 10.20  
 CO<sub>2</sub> (dry volume %): 9.20  
 N<sub>2</sub>+CO (dry volume %): 80.60

Nozzle ID No: 276-1  
 Nozzle Diameter (D<sub>n</sub>): 0.276  
 Probe ID No: M-B-2  
 Pitot C<sub>p</sub>: 0.84  
 Pitot Leak Check:  Pass  Fail

Test Date: 9/21/05  
 Start Time: 08:05  
 Stop Time: 10:20  
 Leak Rate Before: 0.004 cfm @ 15 "Hg  
 Leak Rate After: 0.003 cfm @ 8 "Hg

H<sub>2</sub>O (condensate, ml or gm): 493.5  
 H<sub>2</sub>O (silica, g): 21.0  
 Actual Moisture (%): 21.02

Meter Box ID. No: 66-13  
 Meter ΔH@: 1.79910  
 Meter Y<sub>0</sub>: 0.98700

Traverse Point	Run Time 5.0 min/read	Pitot ΔP <sub>s</sub> (in. H <sub>2</sub> O)	Sample ΔH (in. H <sub>2</sub> O)	Metered (dcf)	Stack T <sub>s</sub> (°F)	Dry Gas Meter		√ΔP <sub>s</sub> (calculated) (√in. H <sub>2</sub> O)	Volume (calculated) (ft <sup>3</sup> )	Isokinetics (calculated) (%)
						T <sub>m-in</sub> (°F)	T <sub>m-out</sub> (°F)			
	0.0			21.550						
1-01	5.0	0.70	2.10	25.660	307	85	83	0.84	4.11	103.0
1-02	10.0	0.33	0.99	28.490	298	87	83	0.57	2.83	102.2
1-03	15.0	0.41	1.20	31.650	303	90	84	0.64	3.16	102.4
1-04	20.0	0.55	1.70	35.350	306	91	85	0.74	3.70	103.7
1-05	25.0	0.80	2.40	39.690	307	93	85	0.89	4.34	100.9
Leak-Check	25.0			39.800						
2-01	30.0	0.75	2.30	44.050	309	92	86	0.87	4.25	102.1
2-02	35.0	0.70	2.10	48.130	308	95	87	0.84	4.08	101.0
2-03	40.0	0.68	2.00	52.140	307	96	87	0.82	4.01	100.5
2-04	45.0	0.60	1.80	55.930	307	96	88	0.77	3.79	101.0
2-05	50.0	0.55	1.70	59.660	304	96	88	0.74	3.73	103.6
Leak-Check	50.0			59.700						
3-01	55.0	0.75	2.30	63.920	308	93	89	0.87	4.22	101.0
3-02	60.0	0.72	2.20	68.100	307	96	89	0.85	4.18	101.7
3-03	65.0	0.63	1.90	71.990	307	97	89	0.79	3.89	101.0
3-04	70.0	0.56	1.70	75.740	305	97	90	0.75	3.75	103.0
3-05	75.0	0.47	1.40	79.085	307	97	90	0.69	3.35	100.4
Leak-Check	75.0			79.195						
4-01	80.0	0.70	2.10	83.290	306	93	90	0.84	4.10	101.2
4-02	85.0	0.77	2.30	87.580	306	97	90	0.88	4.29	100.7
4-03	90.0	0.67	2.00	91.560	309	98	90	0.82	3.98	100.2
4-04	95.0	0.59	1.80	95.400	309	97	90	0.77	3.84	103.1
4-05	100.0	0.54	1.60	99.000	306	97	91	0.73	3.60	100.7
Leak-Check	100.0			99.040						
5-01	105.0	0.18	0.54	101.100	307	94	90	0.42	2.06	100.0
5-02	110.0	0.68	2.00	105.050	306	93	90	0.82	3.95	99.0
5-03	115.0	0.60	1.80	108.820	306	96	90	0.77	3.77	100.2
5-04	120.0	0.55	1.70	112.520	307	96	90	0.74	3.70	102.8
5-05	125.0	0.48	1.40	115.925	307	96	90	0.69	3.41	101.2
Final	125.0		1.80120	94.07500	306.36000		91.24000	0.76667	94.07500	

25 points sampled. Sq. RTAP

QC-Check: Field Averages	0.7667	1.8012	94.0750	306.3600	91.2400
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Avg. OK     Avg. OK     Avg. OK     Avg. OK     Avg. OK

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Field Data Printout

Test Method: USEPA Method 29  
 Analyte: Mercury

Location: Unit 3 FF Outlet  
 Test Run: 5  
 Client: Wheelabrator North Broward, Inc  
 Project No: 9708  
 Source Area (ft<sup>2</sup>): 64.00000

Bar. Press. (in. Hg): 30.50  
 Static P: -12.5

Nozzle ID No: .276-1  
 Nozzle Diameter (D<sub>n</sub>): 0.276  
 Probe ID No: M-B-2  
 Pilot C<sub>p</sub>: 0.84

Test Date: 9/21/05  
 Start Time: 10:43  
 Stop Time: 12:59

O<sub>2</sub> (dry volume %): 10.00  
 CO<sub>2</sub> (dry volume %): 9.20  
 N<sub>2</sub>+CO (dry volume %): 80.80

Pitot Leak Check:  Pass  Fail

Leak Rate Before: 0.004 cfm @ 45 \*Hg  
 Leak Rate After: 0.004 cfm @ 8 \*Hg

H<sub>2</sub>O (condensate, ml or gm): 461.4  
 H<sub>2</sub>O (silica, g): 16.6  
 Actual Moisture (%): 21.40

Meter Box ID. No: 66-13  
 Meter ΔH@: 1.79910  
 Meter Y<sub>c</sub>: 0.98700

Traverse Point	Run Time 5.0 min/road	Pilot ΔP <sub>s</sub> (in. H <sub>2</sub> O)	Sample ΔH (in. H <sub>2</sub> O)	Metered (dcf)	Stack T <sub>s</sub> (°F)	Dry Gas Meter		ΔΔP <sub>s</sub> (calculated) (in. H <sub>2</sub> O)	Volume (calculated) (ft <sup>3</sup> )	Isokinetics (calculated) (%)
						T <sub>m-in</sub> (°F)	T <sub>m-out</sub> (°F)			
	0.0			116.195						
1-01	5.0	0.35	1.00	119.050	298	90	89	0.59	2.86	99.7
1-02	10.0	0.37	1.10	122.400	298	91	89	0.61	3.35	113.7*
1-03	15.0	0.37	1.10	125.010	303	93	89	0.61	2.61	88.7*
1-04	20.0	0.45	1.40	128.390	306	93	89	0.67	3.38	104.5
1-05	25.0	0.53	1.60	132.010	306	94	89	0.73	3.62	103.1
Leak-Check	25.0			132.135						
2-01	30.0	0.62	1.90	136.040	307	93	90	0.79	3.91	102.9
2-02	35.0	0.48	1.40	139.430	306	96	90	0.69	3.39	101.1
2-03	40.0	0.53	1.60	143.040	306	98	91	0.73	3.61	102.2
2-04	45.0	0.60	1.80	146.850	307	99	91	0.77	3.81	101.4
2-05	50.0	0.57	1.70	150.535	308	99	91	0.75	3.69	100.7
Leak-Check	50.0			150.565						
3-01	55.0	0.36	1.10	153.550	307	95	92	0.60	2.99	102.7
3-02	60.0	0.53	1.60	157.180	307	96	92	0.73	3.63	102.9
3-03	65.0	0.53	1.60	160.800	307	98	92	0.73	3.62	102.5
3-04	70.0	0.50	1.50	164.290	308	98	93	0.71	3.49	101.7
3-05	75.0	0.45	1.40	167.660	307	98	93	0.67	3.37	103.4
Leak-Check	75.0			167.765						
4-01	80.0	0.60	1.80	171.550	307	95	92	0.77	3.79	101.0
4-02	85.0	0.55	1.70	175.240	307	98	92	0.74	3.69	102.6
4-03	90.0	0.50	1.50	178.720	306	97	92	0.71	3.48	101.4
4-04	95.0	0.47	1.40	182.080	307	97	92	0.69	3.36	101.0
4-05	100.0	0.47	1.40	185.445	308	98	93	0.69	3.36	101.1
Leak-Check	100.0			185.505						
5-01	105.0	0.42	1.30	188.770	305	96	93	0.65	3.27	103.7
5-02	110.0	0.43	1.30	192.020	304	99	93	0.66	3.25	101.7
5-03	115.0	0.48	1.40	195.420	305	100	94	0.69	3.40	100.6
5-04	120.0	0.55	1.70	199.140	307	99	94	0.74	3.72	103.1
5-05	125.0	0.43	1.30	202.415	307	99	94	0.66	3.28	102.6
Final	125.0		1.46400	85.90000	305.72000	93.96000		0.69469	85.90000	

25 points sampled  
 QC-Check: Field Averages  
 Sq.Rt.ΔP: 0.6947 1.4640 85.9000 305.7200 93.9600  
 Avg. OK  Avg. OK  Avg. OK  Avg. OK  Avg. OK

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Field Data Printout

Test Method: USEPA Method 29  
 Analyte: Mercury

Location: Unit 3 FF Outlet  
 Test Run: 6  
 Client: Wheelabrator North Broward, Inc  
 Project No: 9708  
 Source Area (ft<sup>2</sup>): 64.00000

Bar. Press. (in. Hg): 30.50  
 Static P.: -12.3  
 O<sub>2</sub> (dry volume %): 10.20  
 CO<sub>2</sub> (dry volume %): 9.20  
 N<sub>2</sub>+CO (dry volume %): 80.60

Nozzle ID No: 276-1  
 Nozzle Diameter (D<sub>n</sub>): 0.276  
 Probe ID No: M-8-2  
 Pitot C<sub>p</sub>: 0.84  
 Pitot Leak Check:  Pass  Fail

Test Date: 9/21/05  
 Start Time: 13:15  
 Stop Time: 15:29  
 Leak Rate Before: 0.005 cfm @ 15 "Hg  
 Leak Rate After: 0.005 cfm @ 9 "Hg

H<sub>2</sub>O (condensate, ml or gm): 471.1  
 H<sub>2</sub>O (silica, g): 16.9  
 Actual Moisture (%): 21.76

Meter Box ID. No: 66-13  
 Meter ΔH@: 1.79910  
 Meter Y<sub>g</sub>: 0.98700

Traverse Point	Run Time 5.0 min/read	Pitot ΔP <sub>s</sub> (in. H <sub>2</sub> O)	Sample ΔH (in. H <sub>2</sub> O)	Metered (dct)	Stack T <sub>s</sub> (°F)	Dry Gas Meter		√ΔP <sub>s</sub> (calculated) (√in. H <sub>2</sub> O)	Volume (calculated) (ft <sup>3</sup> )	Isokinetics (calculated) (%)
						T <sub>m-in</sub> (°F)	T <sub>m-out</sub> (°F)			
1-01	5.0	0.28	0.84	202.670	296	95	94	0.53	2.61	101.2
1-02	10.0	0.30	0.90	205.280	296	96	94	0.55	2.69	100.7
1-03	15.0	0.41	1.20	211.130	304	95	94	0.64	3.16	101.9
1-04	20.0	0.50	1.50	214.600	308	97	94	0.71	3.47	101.4
1-05	25.0	0.62	1.90	218.510	308	98	94	0.79	3.91	102.7
Leak-Check	25.0			218.560						
2-01	30.0	0.75	2.30	222.850	309	97	94	0.87	4.29	102.7
2-02	35.0	0.62	1.90	226.790	308	99	94	0.79	3.94	103.4
2-03	40.0	0.53	1.80	230.420	305	100	95	0.73	3.63	102.5
2-04	45.0	0.45	1.40	233.790	307	100	95	0.67	3.37	103.4
2-05	50.0	0.48	1.40	237.165	307	101	95	0.69	3.38	100.2
Leak-Check	50.0			237.220						
3-01	55.0	0.47	1.40	240.610	306	98	96	0.69	3.39	101.8
3-02	60.0	0.51	1.50	244.130	305	101	96	0.71	3.52	101.1
3-03	65.0	0.53	1.60	247.760	306	102	97	0.73	3.63	102.2
3-04	70.0	0.47	1.40	251.160	307	102	97	0.69	3.40	101.7
3-05	75.0	0.42	1.30	254.420	308	101	97	0.65	3.26	103.3
Leak-Check	75.0			254.525						
4-01	80.0	0.63	1.90	258.430	307	99	97	0.79	3.91	101.3
4-02	85.0	0.65	2.00	262.450	307	102	97	0.81	4.02	102.4
4-03	90.0	0.55	1.70	266.180	306	103	97	0.74	3.73	103.1
4-04	95.0	0.53	1.60	269.810	309	103	97	0.73	3.63	102.3
4-05	100.0	0.45	1.40	273.245	310	103	97	0.67	3.44	105.1
Leak-Check	100.0			273.285						
5-01	105.0	0.15	0.45	275.160	310	96	96	0.39	1.88	99.9
5-02	110.0	0.55	1.70	278.860	312	96	96	0.74	3.70	103.4
5-03	115.0	0.55	1.70	282.570	315	98	95	0.74	3.71	103.7
5-04	120.0	0.48	1.40	285.940	325	98	95	0.69	3.37	101.5
5-05	125.0	0.45	1.40	289.300	316	98	95	0.67	3.36	103.9
Final	125.0		1.49560	86.38000	307.88000	97.32000		0.69571	86.38000	

25 points sampled

Sq.Rt.ΔP	0.6957	1.4956	86.3800	307.8800	97.3200
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QC-Check: Field Averages

Avg. OK     Avg. OK     Avg. OK     Avg. OK     Avg. OK

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USEPA Method 3 Laboratory Data

Test Method: USEPA Method 29  
 Analyte: Mercury

Location: Unit 3 FF Outlet  
 Client: Wheelabrator North Broward, Inc  
 Project No: 9708  
 Method: EPA Method 3  
 Fuel Type: Municipal Waste  
 F<sub>o</sub> for Fuel: 1.03 to 1.3

Run Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Percent N <sub>2</sub>	Dry Mol. Weight	F <sub>o</sub>	Method of Analysis: Orsat
4	1	9.2	19.4	10.2	80.6	29.88	1.16304	<i>All measurements in spec.</i>
	2	9.2	19.4	10.2	80.6	29.88		
	3	9.2	19.4	10.2	80.6	29.88		
	Avg.	9.20000		10.20000	80.60000	29.88		
CEM or Other Avg:		9.20000		10.20000	80.60000	29.88000		<input checked="" type="checkbox"/> F <sub>o</sub> value within expected range.

Run Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Percent N <sub>2</sub>	Dry Mol. Weight	F <sub>o</sub>	Method of Analysis: Orsat
5	1	9.2	19.2	10.0	80.8	29.87	1.18478	<i>All measurements in spec.</i>
	2	9.2	19.2	10.0	80.8	29.87		
	3	9.2	19.2	10.0	80.8	29.87		
	Avg.	9.20000		10.00000	80.80000	29.87		
CEM or Other Avg:		9.20000		10.00000	80.80000	29.87200		<input checked="" type="checkbox"/> F <sub>o</sub> value within expected range.

Run Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Percent N <sub>2</sub>	Dry Mol. Weight	F <sub>o</sub>	Method of Analysis: Orsat
6	1	9.2	19.4	10.2	80.6	29.88	1.16304	<i>All measurements in spec.</i>
	2	9.2	19.4	10.2	80.6	29.88		
	3	9.2	19.4	10.2	80.6	29.88		
	Avg.	9.20000		10.20000	80.60000	29.88		
CEM or Other Avg:		9.20000		10.20000	80.60000	29.88000		<input checked="" type="checkbox"/> F <sub>o</sub> value within expected range.

Run Number	Trial	Percent CO <sub>2</sub>	Percent O <sub>2</sub> +CO <sub>2</sub>	Percent O <sub>2</sub>	Percent N <sub>2</sub>	Dry Mol. Weight	F <sub>o</sub>	Method of Analysis: Orsat
	1							
	2							
	3							
	Avg.							
CEM or Other Avg:								<input type="checkbox"/> F <sub>o</sub> value within expected range.

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USEPA Method 4 Laboratory Data

Location: Unit 3 FF Outlet  
 Client: Wheelabrator North Broward, Inc  
 Project No: 9708

Test Method: USEPA Method 29  
 Analyte: Mercury

Test Run:

Contents	Gross (gm)	Tare (gm)	Net (gm)
Impinger 1 Empty	794.0	434.2	359.8
Impinger 2 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	667.1	552.5	114.6
Impinger 3 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	589.3	571.6	17.7
Impinger 4 Empty	441.3	439.5	1.8
Impinger 5 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	529.9	529.7	0.2
Impinger 6 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	559.0	559.8	-0.6
Impinger 7 Silica Gel	770.6	749.6	21.0
Impinger 8			

Rinse:  (ml or gm)

	Field Data Check
493.5 Liquid (gm)	
0.0 less rinse (gm)	
493.5 Net Liquid (gm)	<input checked="" type="checkbox"/> QA/QC OK
+ 21.0 Silica Gel (gm)	<input checked="" type="checkbox"/> QA/QC OK
514.5 Total Vlc (gm)	<input checked="" type="checkbox"/> QA/QC OK

Test Run:

Contents	Gross (gm)	Tare (gm)	Net (gm)
Impinger 1 Empty	806.4	437.9	368.5
Impinger 2 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	597.4	511.9	85.5
Impinger 3 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	526.6	521.5	5.1
Impinger 4 Empty	428.6	427.9	0.7
Impinger 5 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	528.4	527.4	1.0
Impinger 6 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	533.6	533.0	0.6
Impinger 7 Silica Gel	748.5	731.9	16.6
Impinger 8			

Rinse:  (ml or gm)

	Field Data Check
461.4 Liquid (gm)	
0.0 less rinse (gm)	
461.4 Net Liquid (gm)	<input checked="" type="checkbox"/> QA/QC OK
+ 16.6 Silica Gel (gm)	<input checked="" type="checkbox"/> QA/QC OK
478.0 Total Vlc (gm)	<input checked="" type="checkbox"/> QA/QC OK

Test Run:

Contents	Gross (gm)	Tare (gm)	Net (gm)
Impinger 1 Empty	797.0	433.9	363.1
Impinger 2 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	641.7	548.4	93.3
Impinger 3 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	582.9	571.1	11.8
Impinger 4 Empty	442.2	439.8	2.4
Impinger 5 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	561.8	561.8	0.0
Impinger 6 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	532.2	531.7	0.5
Impinger 7 Silica Gel	786.7	769.8	16.9
Impinger 8			

Rinse:  (ml or gm)

	Field Data Check
471.1 Liquid (gm)	
0.0 less rinse (gm)	
471.1 Net Liquid (gm)	<input checked="" type="checkbox"/> QA/QC OK
+ 16.9 Silica Gel (gm)	<input checked="" type="checkbox"/> QA/QC OK
488.0 Total Vlc (gm)	<input checked="" type="checkbox"/> QA/QC OK

Test Run:

Contents	Gross (gm)	Tare (gm)	Net (gm)
Impinger 1 Empty			
Impinger 2 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>			
Impinger 3 5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>			
Impinger 4 Empty			
Impinger 5 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>			
Impinger 6 4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>			
Impinger 7 Silica Gel			
Impinger 8			

Rinse:  (ml or gm)

	Field Data Check
Liquid (gm)	
less rinse (gm)	
Net Liquid (gm)	<input type="checkbox"/> QA/QC OK
Silica Gel (gm)	<input type="checkbox"/> QA/QC OK
Total Vlc (gm)	<input type="checkbox"/> QA/QC OK

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WHEELABRATOR NORTH BROWARD  
POMPANO BEACH, FLORIDA

Client Reference No: 14500124  
CleanAir Project No: 9708-4

**LABORATORY DATA**

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Wheelabrator North Broward, Inc  
 Clean Air Project No: 9708  
 Unit 3 FF Outlet

**USEPA Method 29  
 Mercury (Hg) Laboratory Parameters**

**Blank Analysis**

m <sub>1b-B</sub>	Fraction 1B Blank (µg)	<0.1000
m <sub>2b-B</sub>	Fraction 2B Blank (µg)	<0.3000
m <sub>3a-B</sub>	Fraction 3A Blank (µg)	<0.2000
m <sub>3b-B</sub>	Fraction 3B Blank (µg)	<0.4000
m <sub>3c-B</sub>	Fraction 3C Blank (µg)	<0.4000
m <sub>total-B</sub>	Total Blank Amount (µg)	<1.4000

**Run No.**

	1	2	3
Date (2005)	Sep 20	Sep 20	Sep 20
Start Time (approx.)	08:30	12:04	14:35
Stop Time (approx.)	11:18	14:17	16:50

**Sample Analysis**

m <sub>1b-S</sub>	Fraction 1B Sample (µg)	<0.1000	<0.1000	<0.1000
m <sub>2b-S</sub>	Fraction 2B Sample (µg)	10.0180	10.9757	12.8701
m <sub>3a-S</sub>	Fraction 3A Sample (µg)	<0.2000	<0.2000	<0.2000
m <sub>3b-S</sub>	Fraction 3B Sample (µg)	<0.5000	<0.5000	<0.5000
m <sub>3c-S</sub>	Fraction 3C Sample (µg)	0.8182	<0.4000	<0.4000
m <sub>total-S</sub>	Total Sample Amount (µg)	10.8362	10.9757	12.8701

**Allowable Blank**

m <sub>T-B-allow</sub>	Total Allowable Blank (µg)	0.0000	0.0000	0.0000
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**Sample Corrected for Blank**

m <sub>n</sub>	Total Sample Amount (µg)	10.8362	10.9757	12.8701
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**Sample Corrected for Blank - Prorated Fractions**

m <sub>n-1b</sub>	Fraction 1B Prorated (µg)	<0.1000	<0.1000	<0.1000
m <sub>n-2b</sub>	Fraction 2B Prorated (µg)	10.0180	10.9757	12.8701
m <sub>n-3a</sub>	Fraction 3A Prorated (µg)	<0.2000	<0.2000	<0.2000
m <sub>n-3b</sub>	Fraction 3B Prorated (µg)	<0.5000	<0.5000	<0.5000
m <sub>n-3c</sub>	Fraction 3C Prorated (µg)	0.8182	<0.4000	<0.4000

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# **Clean Air Engineering, Inc.**

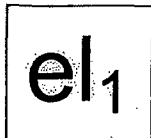
500 West Wood Street  
Palatine, IL 60067

Project Number: 9708

Mercury

EPA Method 29 Analysis

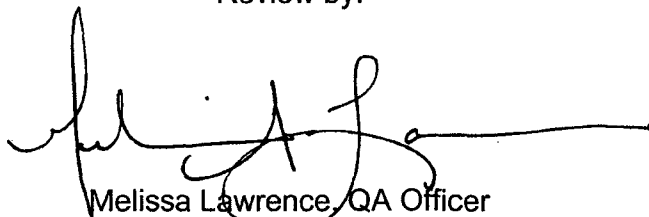
Analytical Report  
5934



Element One, Inc.  
5022-C Wrightsville Av., Wilmington, NC 28403  
910-793-0128 FAX: 910-792-6853 e1lab@e1lab.com

The following data for Analytical Report 5934  
has been reviewed for completeness, accuracy,  
adherence to method protocol,  
and compliance with quality assurance guidelines.

Review by:

A handwritten signature in black ink, appearing to read 'Melissa Lawrence', with a long horizontal flourish extending to the right.

Melissa Lawrence, QA Officer  
September 30, 2005

Report Reviewed and Finalized By:

Ken Smith, Laboratory Director  
September 30, 2005

**elementOne**

5934 Clean Air-IL M29 Report Packet  
Page 2 of 14

# SUMMARY OF RESULTS

**elementOne**

5934 Clean Air-IL M29 Report Packet  
Page 3 of 14

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## Summary of Analysis

### Boiler #6 Summary of Method 29 Mercury Analysis

Run Number		Average Total Catch, µg	Front half µg	H <sub>2</sub> O <sub>2</sub> / HNO <sub>3</sub> µg	Empty Impinger µg	KMnO <sub>4</sub> µg	HCl µg
U3 FF Outlet R1	#1	10.8	< 0.1	10.0	< 0.2	< 0.5	0.80
	#2		< 0.1	10.0	< 0.2	< 0.5	0.84
U3 FF Outlet R2	#1	11.0	< 0.1	11.0	< 0.2	< 0.5	< 0.4
	#2		< 0.1	10.9	< 0.2	< 0.5	< 0.4
U3 FF Outlet R3	#1	12.9	< 0.1	12.8	< 0.2	< 0.5	< 0.4
	#2		< 0.1	12.9	< 0.2	< 0.5	< 0.4
Field Blank	#1	< 0.5	< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
	#2		< 0.1	< 0.3	< 0.2	< 0.5	< 0.4
Reagent Blank	#1	< 0.4	< 0.1	< 0.3	< 0.2	< 0.4	< 0.4
	#2		< 0.1	< 0.3	< 0.2	< 0.4	< 0.4

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# ANALYTICAL NARRATIVE

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## Element One Analytical Narrative

Client:	Clean Air Engineering, IL	Element One #:	5934
Client ID:	Wheelabrator, N. Broward	Analyst:	CML, IJJ
Method:	M29	Dates Received:	9/23/05
Analytes:	Hg	Dates Analyzed:	9/27-30/05

### Summary of Analysis

The Method 29 samples were digested, prepared, and analyzed according to Method 29 protocol. Samples were analyzed for mercury on a PerkinElmer FIMS-100 CVAA mercury analyzer.

### Detection Limits

The FIMS-100 CVAA instrument reporting limit for mercury was 0.004 µg per aliquot analyzed.

### Analysis QA/QC

Duplicate analyses relative percent difference (RPD) and spike sample recovery data are summarized in the Quality Control Section. All QA/QC data was within the criteria of the method.

### Additional Comments

The reported results have not been corrected for any blank values or spike recovery values. Nothing unusual was noticed with any of the samples or analyses.

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# QUALITY CONTROL SUMMARY

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## Summary of Quality Control Data

### Mercury Duplicate Analysis RPD

*(Method 29 QC limits: <10% for RPD)*

Run Number	Front half	H2O2/HNO4	Empty Impinger	KMnO4	HCl
U3 FF Outlet R1	NA	0.1%	NA	NA	4.3%
U3 FF Outlet R2	NA	0.6%	NA	NA	NA
U3 FF Outlet R3	NA	0.9%	NA	NA	NA
Field Blank	NA	NA	NA	NA	NA
Reagent Blank	NA	NA	NA	NA	NA

### Mercury Spike Recoveries

*(Method 29 QC limits: ±25% for Spike Recoveries)*

Run Number		Front half	H2O2/HNO4	Empty Impinger	KMnO4	HCl
U3 FF Outlet R3	#1	121%	95%	102%	102%	88%
	#2	121%	95%	102%	100%	90%

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# SAMPLE CUSTODY

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**CHAIN OF CUSTODY FORM**

5934

CLIENT Wheelabrator North Broward  
 PLANT Same  
 PROJECT MANAGER Scott Brown

PROJECT NO. 9708  
 DEPT. 66

ANALYSIS REQUESTED

NO. OF CONTAINERS

ORIGINAL VOLUME

**COPY**


ADDITIONAL INFORMATION

*EPA METHOD 29 FOR Hg*

CLEANAIR  
 LAB NO. RUN NO. TEST LOCATION DATE SAMPLE MATRIX

LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX	NO. OF CONTAINERS	ORIGINAL VOLUME	ANALYSIS REQUESTED	ADDITIONAL INFORMATION
	1	Unit 3 FF Outlet	9/20	Filter	1	X		
	1			Front-Half 0.1N HNO3 Rinse	1	X		
	1			Imp. 1,2,3 + 0.1N HNO3 Rinse	1	X		
	1			Imp. 4 + 0.1N HNO3 Rinse	1	X		
	1			Imp. 5,6 KMnO4+H2O Rinse	1	X		
	1		↓	Imp. 5,6 HCl Rinse	1	X		
	2		9/20	Filter	1	X		
	2			Front-Half 0.1N HNO3 Rinse	1	X		
	2			Imp. 1,2,3 + 0.1N HNO3 Rinse	1	X		
	2			Imp. 4 + 0.1N HNO3 Rinse	1	X		
	2			Imp. 5,6 KMnO4+H2O Rinse	1	X		
	2	V	↓	Imp. 5,6 HCl Rinse	1	X		

Relinquished by: (Signature) <i>D. Dreska</i>	Date / Time	Received by: (Signature) <i>[Signature]</i>	Date / Time 9/23/05 10:00	Relinquished by: (Signature)	Date / Time
Courier: <i>Fed Ex</i>	Date / Time	Relinquished by: (Signature) <i>[Signature]</i>	Date / Time	Received for Analysis by: <i>Element One</i>	Date / Time 9/23/05 10:00

Special Handling Instructions	This form was completed by: Dick Dreska Signature <i>[Signature]</i> Date 9/22/05	 500 West Wood Street Palatine, IL 60067 (800) 627-0033 ph (847) 991-3385 fax www.cleanair.com <small>LDS001A_1-COC Palatins_M29, Jul 2002                  Copyright © 2002 Clean Air Engineering Inc.</small>
Forwarding Lab: <u>Element One</u> <u>Wilmington, NC 28403</u>	PO Number: _____	

CHAIN OF CUSTODY FORM

5934

CLIENT Wheelabrator North Broward  
 PLANT Same  
 PROJECT MANAGER Scott Brown

PROJECT NO. 9708  
 DEPT. 66

NO. OF CONTAINERS

ORIGINAL VOLUME

ANALYSIS REQUESTED

COPY

ADDITIONAL INFORMATION

CLEANAIR

LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX	NO. OF CONTAINERS	ORIGINAL VOLUME	Hg	Archive	ADDITIONAL INFORMATION
	3	Unit 3 FF Outlet	9/20	Filter	1		X		
	3			Front-Half 0.1N HNO3 Rinse	1		X		
	3			Imp. 1,2,3 + 0.1N HNO3 Rinse	1		X		
	3			Imp. 4 + 0.1N HNO3 Rinse	1		X		
	3			Imp. 5,6 KMnO4+H2O Rinse	1		X		
	3		X	Imp. 5,6 HCl Rinse	1		X		
	4		9/21	Filter	1			X	
	4			Front-Half 0.1N HNO3 Rinse	1			X	
	4			Imp. 1,2,3 + 0.1N HNO3 Rinse	1			X	
	4			Imp. 4 + 0.1N HNO3 Rinse	1			X	
	4			Imp. 5,6 KMnO4+H2O Rinse	1			X	
	4	V		Imp. 5,6 HCl Rinse	1			X	

Relinquished by: (Signature)	Date / Time	Received by: (Signature)	Date / Time	Relinquished by: (Signature)	Date / Time
		<i>[Signature]</i>	9-23-05 10:00		
Courier: <i>Fed Ex</i>	Date / Time	Relinquished by: (Signature)	Date / Time	Received for Analysis by: <i>Element One</i>	Date / Time
		<i>[Signature]</i>			9-23-05 10:00

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Wilmington, NC 28403

PO Number: \_\_\_\_\_

This form was completed by:

Dick Dreska  
 Signature *[Signature]* Date 9/23



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CHAIN OF CUSTODY FORM


5934

CLIENT Wheelabrator North Broward PROJECT NO. 9708  
 PLANT Same DEPT. 66  
 PROJECT MANAGER Scott Brown

ANALYSIS REQUESTED  
 NO. OF CONTAINERS  
 ORIGINAL VOLUME  
 Hg  
 Archive  
**COPY**  
 ADDITIONAL INFORMATION

CLEANAIR LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX	NO. OF CONTAINERS	ORIGINAL VOLUME	Hg	Archive	ANALYSIS REQUESTED	ADDITIONAL INFORMATION
	5	Unit 3 FF Outlet	9/21	Filter	1			X		
	5		↓	Front-Half 0.1N HNO3 Rinse	1			X		
	5			Imp. 1,2,3 + 0.1N HNO3 Rinse	1			X		
	5			Imp. 4 + 0.1N HNO3 Rinse	1			X		
	5			Imp. 5,6 KMnO4+H2O Rinse	1			X		
	5			Imp. 5,6 HCl Rinse	1			X		
	6			9/21	Filter	1			X	
	6		↓	Front-Half 0.1N HNO3 Rinse	1			X		
	6			Imp. 1,2,3 + 0.1N HNO3 Rinse	1			X		
	6			Imp. 4 + 0.1N HNO3 Rinse	1			X		
	6			Imp. 5,6 KMnO4+H2O Rinse	1			X		
	6	V		Imp. 5,6 HCl Rinse	1			X		

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 Courier: Fed Ex Date / Time \_\_\_\_\_ Relinquished by: (Signature) \_\_\_\_\_ Date / Time \_\_\_\_\_ Received for Analysis by: Element One Date / Time 9/23/05 10:00

Special Handling Instructions \_\_\_\_\_ Forwarding Lab: Element One  
Wilmington, NC 28403  
 PO Number: \_\_\_\_\_  
 This form was completed by: Dick Dreska Signature [Signature] Date 9/27  
  
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 Palatine, IL 60067  
 (800) 627-0033 ph  
 (847) 991-3385 fax  
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CHAIN OF CUSTODY FORM

5934

CLIENT Wheelabrator North Broward  
 PLANT Same  
 PROJECT MANAGER Scott Brown

PROJECT NO. 9708  
 DEPT. 66

NO. OF CONTAINERS

ORIGINAL VOLUME

ANALYSIS REQUESTED

COPY

ADDITIONAL INFORMATION

CLEANAIR  
 LAB NO. RUN NO. TEST LOCATION DATE SAMPLE MATRIX

LAB NO.	RUN NO.	TEST LOCATION	DATE	SAMPLE MATRIX	NO. OF CONTAINERS	ORIGINAL VOLUME	Hg							
	NA	Field Blank	9/21	Filter	1		X							
	NA			Front-Half 0.1N HNO3 Rinse	1		X							
	NA			Imp. 1,2,3 + 0.1N HNO3 Rinse	1		X							
	NA			Imp. 4 + 0.1N HNO3 Rinse	1		X							
	NA			Imp. 5,6 KMnO4+H2O Rinse	1		X							
	NA	V	↓	Imp. 5,6 HCl Rinse	1		X							
	NA	Reagent Blanks	9/20	3 Quartz Filters	1	NA	X							
	NA			0.1 N HNO3	1	300	X							
	NA			DI H2O	1	100	X							
	NA			5% HNO3 / 10% H2O2	1	200	X							
	NA			4% KMnO4 / 10% H2SO4	1	100	X							
	NA	V	↓	8N HCl / DI H2O	1	225	X							

Relinquished by: (Signature)	Date / Time	Received by: (Signature)	Date / Time	Relinquished by: (Signature)	Date / Time
		<i>[Signature]</i>	9-23-05 10:00		
Courier: <i>Fed Ex</i>	Date / Time	Relinquished by: (Signature)	Date / Time	Received for Analysis by: <i>Element One</i>	Date / Time
		<i>[Signature]</i>			9-23-05 10:00


Special Handling Instructions

Forwarding Lab: Element One  
Wilmington, NC 28403

PO Number: \_\_\_\_\_

This form was completed by:

Dick Dreska  
 Signature *[Signature]* Date 9/22



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# ANALYTICAL DATA

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5934 Clean Air-IL M29 Report Packet

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Project ID/ Number: Wheelabrator, N. Broward 9708

Client: <b>Clean Air IL</b>	Date / Time Received: 9.23.05 / 1000
-----------------------------	--------------------------------------

HNO <sub>3</sub> Lot: <b>1104120</b>	HF Lot: <b>510460</b> <sup>193</sup> <del>41109040</del> <sub>9-26-05</sub>	HCl Lot: <b>41104090</b>	Ref. Method: <b>29</b>
Volume Marked <b>(Y)</b> / N	Volume Loss <b>(N)</b> / ?	pH < 2.0 <b>(Y)</b> / N	

Sample Identification		Sample Identification	
1	U3 FF Outlet R1	7	U3 FF Outlet R4
2	U3 FF Outlet R2	8	U3 FF Outlet R5
3	U3 FF Outlet R3	9	U3 FF Outlet R6
4	U3 FF Outlet R3 Spike	10	U3 FF Outlet R6 Spike
5	Field Blank		
6	Reagent Blank		

Analyses Requested	Samples 1-6	Hg
Analyses Requested	Samples 7-10	Archive

SAMPLE	Front Half		Back Half			HNO <sub>3</sub> (A)		KMnO <sub>4</sub> (B)		HCl (C)	
	BV, ml	FV, ml	BV, ml	Used	FV, ml	BV, ml	FV, ml	BV, ml	FV, ml	BV, ml	FV, ml
1	168	100	900	—	—	110	200	360	500	240	400
2	146	↓	880	—	—	106	↓	355	↓	255	↓
3/4	168	↓	880	—	—	108	↓	370	↓	265	↓
5	169	↓	330	—	—	110	↓	365	↓	230	↓
7											
8											
9/10											

5934-6 REAGENT BLANK			BV, ml	FV, ml	Comments
C-8A	A		200	200	
C-8A	FH & A	0.1N HNO <sub>3</sub>	100	100	
C-8B	B	DI H <sub>2</sub> O	—	—	
C-9	BH	5% HNO <sub>3</sub> /10% H <sub>2</sub> O <sub>2</sub>	280	—	
C-10	B	4% KMnO <sub>4</sub> /10% H <sub>2</sub> SO <sub>4</sub>	100 ml KAO calculate 33 ml DI as 400 ml	—	
C-11	C	8N HCl	225	400	
C-12	FH	Filter	—	100	

Request by \_\_\_\_\_ to analyze Archived Samples 7-10 Due Date \_\_\_\_\_  
 Received by \_\_\_\_\_ Date \_\_\_\_\_





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**METHODOLOGY**

4-3

**VELOCITY AND VOLUMETRIC FLOW RATE - EPA METHOD 2**

EPA Method 2 was used, in conjunction with the wet method testing, to determine the gas velocity and flow rate at the FF Outlet test location.

Each set of velocity determinations included the measurement of gas velocity pressure and gas temperature at each of the EPA Method 1 traverse points. The velocity pressures were measured with a Type S pitot tube. Gas temperature measurements were made using a Type K thermocouple and digital pyrometer. Figure 4-2 includes the components of the EPA Method 2 sampling apparatus.

**GAS COMPOSITION AND MOLECULAR WEIGHT - EPA METHOD 3B**

In order to determine the oxygen (O<sub>2</sub>) concentration, carbon dioxide (CO<sub>2</sub>) concentration and gas molecular weight, a time-integrated sample of the gas was obtained for each sampling train and analyzed in accordance with EPA Method 3B. The gas sample was collected into a vinyl sample bag from isokinetic test methods. The contents of the bag was analyzed for O<sub>2</sub> and CO<sub>2</sub> concentrations using an Orsat gas analyzer.

**MOISTURE CONTENT - EPA METHOD 4**

The flue gas moisture content at each of the test locations was determined in accordance with EPA Method 4, in conjunction with the mercury testing. Figure 4-2 includes the components of the EPA Method 4 sampling apparatus. The gas moisture was determined by quantitatively condensing the moisture in chilled impingers. The amount of moisture condensed was determined gravimetrically. A dry gas meter was used to measure the volume of gas sampled. The amount of water condensed and the volume of gas sampled were used to calculate the gas moisture content in accordance with EPA Method 4.

## METHODOLOGY

4-4

### MERCURY EMISSIONS - EPA METHOD 29

EPA Method 29 was used to measure mercury emissions at the Unit 3 FF Outlet. This method defines metal emissions as particulate and gaseous material isokinetically withdrawn through a temperature controlled probe and collected on a high-efficiency filter and in acidified absorbing solutions.

Figure 4-2 illustrates the EPA Method 29 sampling train which was used. The sampling apparatus contained a glass-lined temperature-controlled probe equipped with a pitot tube (for measuring stack flow rate) and a sharp-edged glass button-hook nozzle. The exit of the probe was connected to a high efficiency quartz fiber filter (Pallflex 2500QAT-UP) supported in a glass filter holder inside an oven. The exit of the filter holder connected directly to a series of seven full size impingers.

The first impinger of the sampling train was left empty to accommodate collection of the flue gas moisture. The second and third impingers of the sampling apparatus each contained 100 milliliters of 5% nitric acid/10% hydrogen peroxide solution. The fourth impinger was left empty. The fifth and sixth impingers each contained 100 milliliters of 4% potassium permanganate/10% sulfuric acid solution. The seventh impinger contained 200 to 300 grams of silica gel. All of the impingers were maintained at a temperature below 68°F for the duration of each test.

Procedures for selecting sampling locations and for the operation of the apparatus were derived from EPA Method 29 and associated EPA Methods 1 through 5. The entire sampling apparatus was leak-checked before and after each test run. Sampling was performed at an average isokinetic rate greater than 90% and less than 110%.

At the conclusion of each test run, the probe and nozzle was rinsed and brushed with 0.1 Normal nitric acid to remove any particulate matter. These rinses were collected into polyethylene sample containers. The quartz fiber filter was recovered and placed into a polyethylene sample container. The volume of liquid collected in each of the impingers was quantified.

The liquid from the first three impingers was transferred to a leak-free polyethylene storage container. The back-half of the filter housing, the first three impingers and all connecting glassware were rinsed with 0.1 Normal nitric acid which was be added to the storage container.

**METHODOLOGY**

4-5

**MERCURY EMISSIONS (CONTINUED)**

Any liquid collected in the fourth impinger was transferred to a separate polyethylene container, and the impinger was rinsed into the same container with 0.1 Normal nitric acid. The contents of impingers 5 and 6 were collected into an amber glass container. Both impingers 5 and 6 and the connecting glassware were then rinsed with acidified potassium permanganate followed by distilled water. These rinses were collected in the glass container. Any residual potassium permanganate retained by the impingers was removed using a rinse of 8 Normal hydrochloric acid, which was collected into a separate glass container. 200 milliliters of distilled water was used to rinse impingers 5 and 6 and added to the same container to also dilute the acid.

All containers were sealed, labeled and liquid levels marked prior to transport to the laboratory. The silica gel weight and the volume of condensate collected in the impingers were used to determine moisture content of the stack gas.

The nitric acid probe rinses, and samples recovered from impingers 1 through 3 were reduced to near dryness and digested with hydrofluoric acid and concentrated nitric acid. The filter was digested with hydrofluoric and nitric acids. The samples obtained from Impingers 4, 5 and 6 were digested separately with acidified potassium permanganate and subsequently analyzed only for mercury. The digested samples were analyzed by cold vapor atomic absorption spectroscopy (CVAAS per Method 7470 in EPA publication SW 846) for mercury by Element One, Inc of Wilmington, North Carolina.



**METHODOLOGY**  
**MERCURY EMISSIONS (CONTINUED)**

4-6

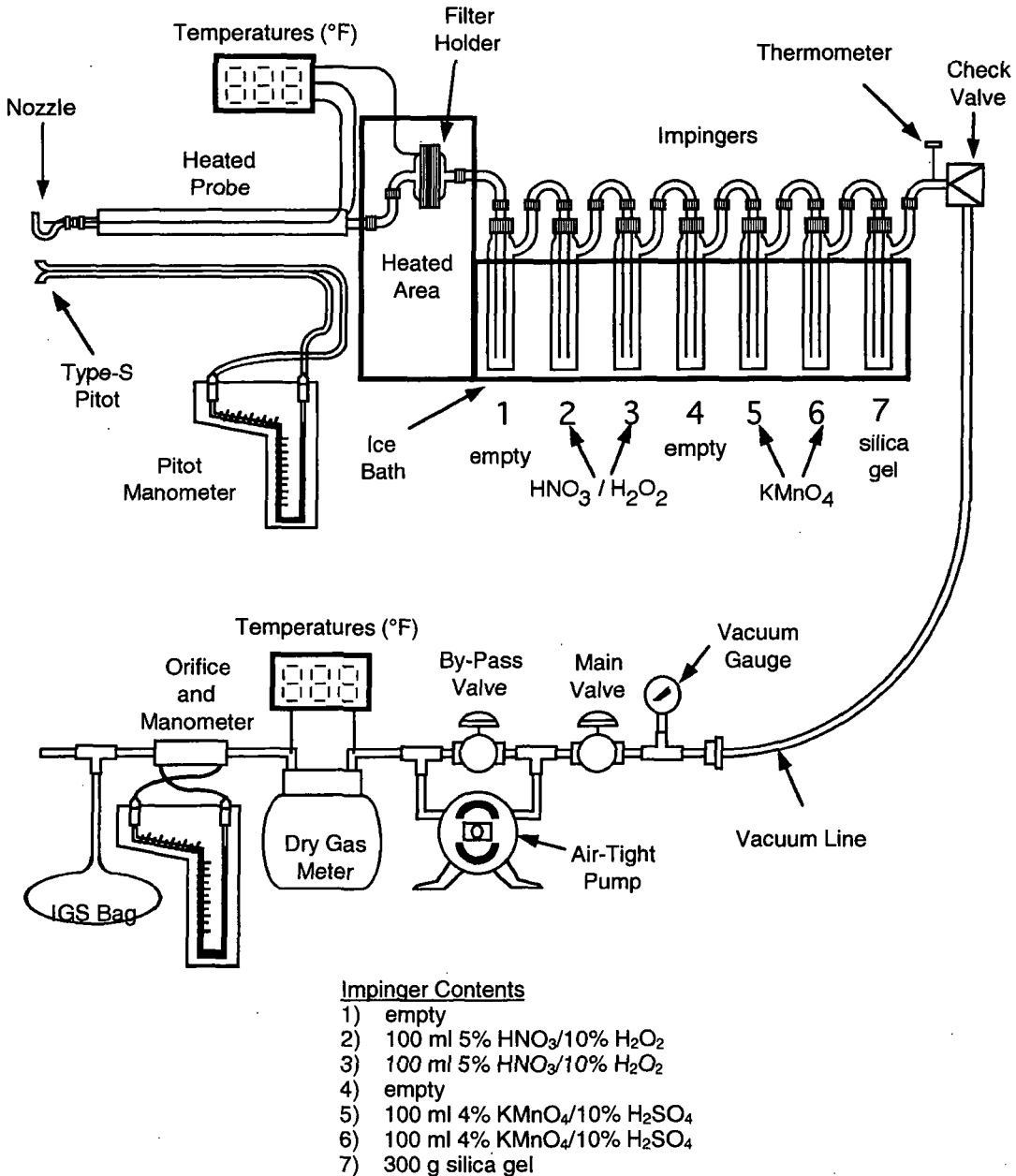


Figure 4-2: Metals Sampling Apparatus (EPA Method 29)

WHEELABRATOR NORTH BROWARD  
POMPANO BEACH, FLORIDA

Client Reference No: 14500124  
CleanAir Project No: 9708-4

**METHODOLOGY**

4-7

**QUALITY ASSURANCE AND QUALITY CONTROL**

All testing followed the EPA quality assurance and quality control guidelines as outlined in the respective methods. Field blanks and matrix spikes for the mercury testing were done as shown in the following Table 4-3. The results of the analysis are shown in Table 2-2.

**Table 4-3:  
Method Field Blanks and Matrix Spikes**

---

<u>Method</u>	<u>Reagent Blank Sets</u>	<u>Field Blank</u>	<u>Duplicate Analysis</u>	<u>Matrix Spikes</u>
EPA M29	1	1	On all analysis	1 predigested filter blank and 1 postdigested sample

---

**DESCRIPTION OF INSTALLATION**

3-2

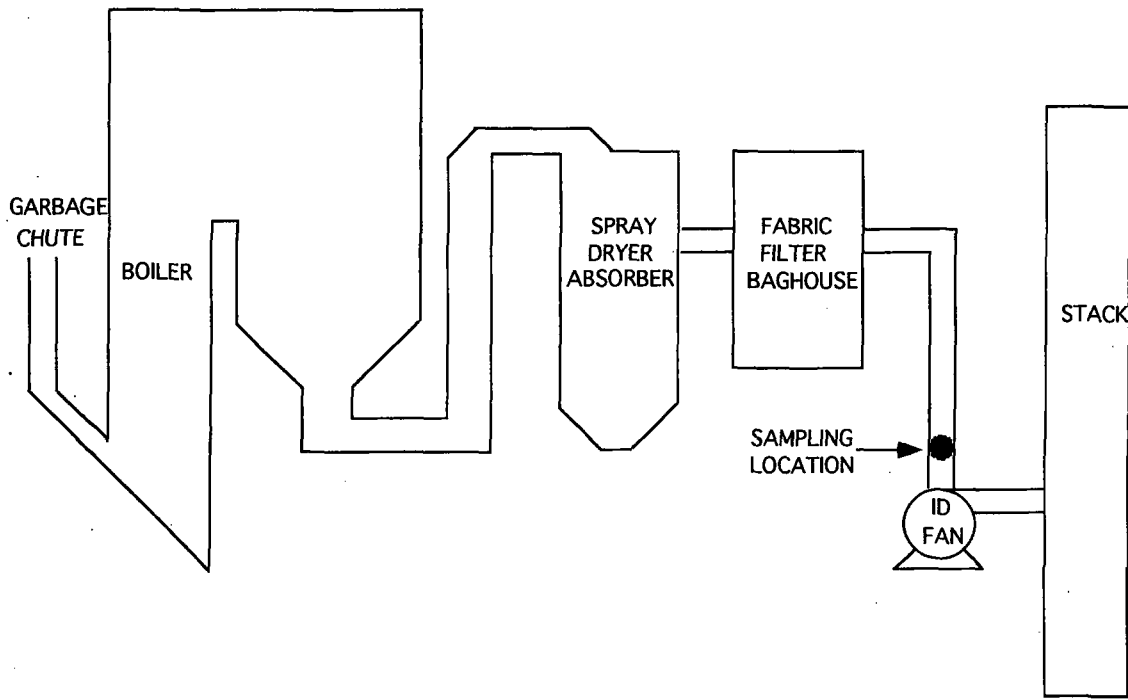


Figure 3-2: Process Schematic

**METHODOLOGY**

The sampling followed procedures as detailed in U.S. Environmental Protection Agency (EPA) Methods 1, 2, 3, 3B, 4 and 29. The following table summarizes the methods and their respective sources.

**Table 4-1:  
Summary of Sampling Procedures**

<u>Title 40 CFR Part 60 Appendix A</u>	
Method 1	"Sample and Velocity Traverses for Stationary Sources"
Method 2	"Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)"
Method 3	"Gas Analysis for the Determination of Dry Molecular Weight"
Method 3B	"Gas Analysis for the Determination of Emission Rate Correction Factor or Excess Air"
Method 4	"Determination of Moisture Content in Stack Gases"
Method 29	"Determination of Metals Emissions from Stationary Sources"

These methods appear in detail in Title 40 of the Code of Federal Regulations (CFR) and on the World Wide Web at <http://www.cleanair.com>.

These sampling, recovery and analytical procedures are summarized on pages 4-1 through 4-7.

The sampling nozzles were calibrated on site. All other equipment was calibrated at the Clean Air Engineering laboratory prior to shipment to the job site. A post-test calibration was performed on the meter boxes at the conclusion of testing to verify that calibration was maintained throughout the test program. Calibration sheets can be found in Appendix Section C.

**SAMPLING POINT DETERMINATION - EPA METHOD 1**

Sampling point locations were determined according to EPA Method 1.

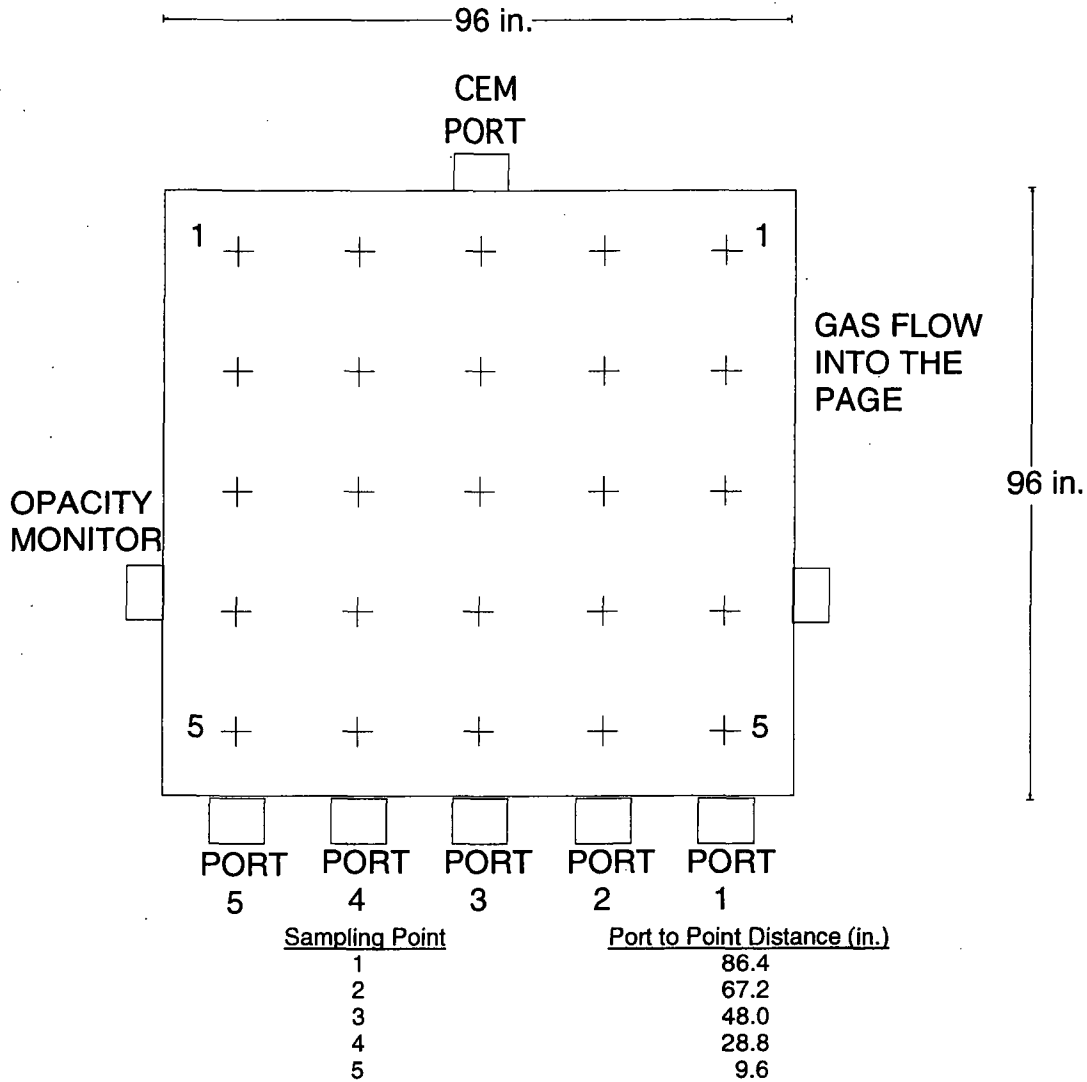
Table 4-2 outlines the sampling point configurations. Figure 4-1 illustrates the sampling points and orientation of sampling ports for the source tested in the program.

**Table 4-2:  
Sampling Points**

Location	Run	Points	Minutes	Total	
Constituent	Method	No. Ports	per Port	per Point	Minutes Figure
<u>Unit 3 FF Outlet</u>					
Mercury	29	1-3 5	5	5	125 4-1

**METHODOLOGY**  
**SAMPLING POINT DETERMINATION (CONTINUED)**

4-2



Diameters upstream from disturbance: 2 diameters      Limit: 2  
Diameters downstream from disturbance: 0.5 diameters      Limit: 0.5

Figure 4-1: Unit 3 FF Outlet - Sampling Point Determination (EPA Method 1)

**Wheelabrator  
NORTH BROWARD  
Emission Test Log**

Date: 21-09-05  
Start Time: 08:05  
End Time: 10:25

SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS
-------------------	--------------------	--------------------	-------------------	---------------	--------------	----------------	----------	-------------------

	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O
Unit 1	512.19	315.66	41.78	32.59	9.20	16.01	295.83	5.74	-12.62
Unit 2	509.57	315.05	42.22	33.94	8.28	15.79	297.02	6.29	-10.57
Unit 3	521.22	314.88	46.87	38.58	8.29	14.20	305.64	6.26	-7.31

G - 7

FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNCR CHEM FLOW	STEAM FLOW
------------------	---------------------	-------------------	-----------------	------------------	-------------------	----------------	-------------------	---------------

	KLBS/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBS/hr
Unit 1	190.54	881.62	828.46	84.56	-0.10	267.02	1173.75	2.91	183.55
Unit 2	188.51	887.65	829.18	85.52	-0.10	269.12	1046.16	6.85	184.12
Unit 3	191.45	891.16	830.42	84.44	-0.09	276.21	1126.26	0.98	183.23

**Wheelabrator  
NORTH BROWARD  
Emission Test Log**

Date: 21-09-05  
Start Time: 10:44  
End Time: 12:59

SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS
-------------------	--------------------	--------------------	-------------------	---------------	--------------	----------------	----------	-------------------

	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O
Unit 1	516.00	315.00	43.36	30.76	12.60	14.07	296.77	5.31	-11.93
Unit 2	506.83	314.91	40.88	28.56	12.32	14.92	297.04	6.27	-10.35
Unit 3	512.87	314.79	42.63	33.07	9.56	14.32	305.18	6.27	-7.04

0  
1  
∞

FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNCR CHEM FLOW	STEAM FLOW
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	KLBs/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBs/hr
Unit 1	190.93	882.00	828.54	83.84	-0.10	267.80	1186.55	3.00	184.10
Unit 2	188.81	887.66	829.09	83.73	-0.10	269.99	1055.02	6.83	184.26
Unit 3	192.95	891.51	830.65	79.65	-0.09	277.06	1133.31	3.07	184.73

**Wheelabrator  
NORTH BROWARD  
Emission Test Log**

Date: 21-09-05  
Start Time: 13:16  
End Time: 15:26

SDA INLET TEMP	SDA OUTLET TEMP	TOTAL SLURRY FL	DIL WATER FLOW	TOTAL LIME	LIME CONC	FF OUT TEMP	FF DP	ID INLET PRESS
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	DEG F	DEG F	GPM	GPM	GPM	%	DEG F	" H2O	" H2O
Unit 1	516.04	315.22	42.76	29.79	12.97	14.77	296.42	5.65	-11.71
Unit 2	505.78	314.91	39.04	28.14	10.90	16.10	297.71	6.28	-10.16
Unit 3	512.71	318.17	41.67	31.75	9.92	15.31	307.67	6.21	-7.18

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6

FEED H2O FLOW	SH OUT STM PRESS	FINAL STM TEMP	TOT AIR FLOW	FURNACE DRAFT	ECONO OUT TEMP	SH ROLL AVG	SNCR CHEM FLOW	STEAM FLOW
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	KLBS/hr	DEG F	DEG F	KSCFM	" H2O	DEG F	DEG F	GPH	KLBS/hr
Unit 1	190.22	882.10	830.63	83.58	-0.09	267.90	1191.84	4.08	183.40
Unit 2	188.72	887.24	828.30	83.06	-0.10	270.03	1053.63	6.69	184.14
Unit 3	192.40	891.11	830.70	78.07	-0.09	277.22	1141.78	2.55	184.16



CONTROL ROOM STACK TEST LOG

Date: 9-21-05

Unit	Test	Run #	Start Time	End Time	Slurry S.G.
3	Mercury	4	0805	1025	
3	Mercury	5	1044	1259	
3	Mercury	6	1316	1526	

CONTROL ROOM STACK TEST LOG

Date: 9-20-05

Unit	Test	Run #	Start Time	End Time	Slurry S.G.
3	Mercury	1	0830	0945	
3	Mercury	1	1017	1118	
3	Mercury	2	1204	1417	
3	Mercury	3	1435	16:50	

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