

AIR CONSTRUCTION PERMIT APPLICATION Medula co.19 **FOR THE** FLORIDA POWER & LIGHT COMPANY LAUDERDALE COMBUSTION TURBINE **PROJECT**

BROWARD COUNTY, FLORIDA

JUL 3 1 2013 Line Cor AIR RESOURCE MANAGEMENT

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Submitted To:

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July 2013

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RESOURCE MANAGEMENT

July 30, 2013

Jeffery Koerner, P.E., Program Administrator Office of Permitting and Compliance Division of Air resource Management Department of Environmental Protection 2600 Blair Stone Road Tallahassee, FL 32399

Droject 0110037-011-AC

Re:

FPL Lauderdale and Fort Myers Combustion Turbine (CT) Projects

Air Construction Permit Application

Dear Mr. Koerner:

Please find enclosed the Air Construction Permit Applications prepared by Golder Associates for Florida Power & Light Company's (FPL) Lauderdale and Fort Myers CT Projects located in Broward and Lee Counties, respectively. As discussed in FPL's June 3, 2013 letter from Randall LaBauve to Brian Accardo, the enclosed Applications are being filed as part of a plan for Fort Myers, Lauderdale, and Port Everglades Plants to bring off-site concentrations below the new 1-hour NO₂ National Ambient Air Quality Standard (NAAQS). The air quality analyses contained in the Applications demonstrate that retiring 48 existing gas turbines at the Fort Myers, Lauderdale, and Port Everglades Plants and replacing this first-generation combustion technology with new, highly efficient combustion turbines at the Lauderdale and Fort Myers Plants will demonstrate compliance with the 1-hour NO₂ NAAQS. For GHG emissions, FPL will separately file at a later date a Prevention of Significant Deterioration (PSD) application for each Project with the U.S. Environmental Protection Agency (EPA) Region IV, as instructed on the Department's website.

If you have any comments or questions regarding the attached Applications, please feel free to contact me at (561) 691-2808 or Ken Proctor at (561) 691-7068.

Sincerely,

Florida Power & Light Company

Matthew J. Raffenberg

Director of Environmental Licensing and Permitting

Environmental Services Department

cc: Brian Accardo, FDEP

Randall LaBauve, FPL

Ken Kosky, Golder Associates Peter Cocotos, Esq., FPL



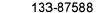
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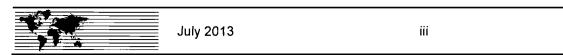
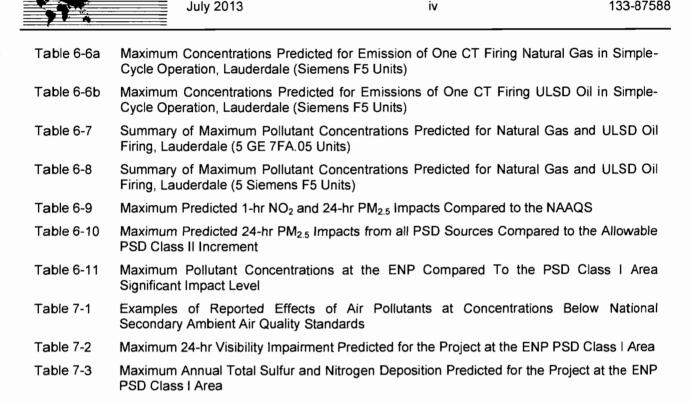


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List of Acronyms

°C degrees Celsius

°F degrees Fahrenheit

µg/m³ micrograms per cubic meter
AAQS Ambient Air Quality Standards

AERMOD American Meteorological Society and U.S. Environmental Protection Agency Regulatory

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Model

AOR Annual Operating Report AQRV air quality related value

BACT Best Available Control Technology
BPIP Building Profile Impact Program
Btu/lb British thermal unit per pound

Btu/kWh British thermal unit per kilowatt hour

Btu/scf British thermal unit per standard cubic foot

CAA Clean Air Act

CEM continuous emissions monitoring

cf/yr cubic foot per year

CFR Code of Federal Regulations

CH₄ methane

CO carbon monoxide CO₂ carbon dioxide

CO₂e carbon dioxide equivalent

CT combustion turbine
DLE dry low emissions

ENP Everglades National Park

EPA U.S. Environmental Protection Agency

F.A.C. Florida Administrative Code

FDEP Florida Department of Environmental Protection

FGT Florida Gas Transmission Company, LLC

FIU Florida International University

FPL Florida Power & Light

ft foot

FR Federal Register

FFFSGU fossil fuel fired steam generating unit g/bhp-hr grams per brake horsepower-hour

g/s grams per second

GEP Good Engineering Practice

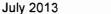
gr/100 scf grains per 100 standard cubic feet

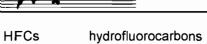
GT Gas Turbines, (typically referred to the older existing machines on the Project Site)

GHG greenhouse gas

HAP hazardous air pollutant







HHV higher heating value

hp horsepower hr/yr hours per year

HRSG heat recovery steam generator

HSH highest, second highest

Hz hertz

1 Interstate highway **ICW** Intracoastal Waterway

km · kilometer kW kilowatt

lb/hr pound per hour

ib/MMBtu pound per million British thermal units

lb/MW-hr pound per megawatt-hour

LHV lower heating value

m meter

MACT Maximum Available Control Technology MMBtu/hr million British thermal units per hour

MMcf/hr million cubic feet per hour MPS Mitsubishi Power Systems

MW megawatt

NAAQS National Ambient Air Quality Standards

NAD83 North American Datum 83

NESHAP National Emission Standards for Hazardous Air Pollutants

N₂O nitrous oxide nitrogen dioxide NO₂ NO_x nitrogen oxides NP National Park

NSPS New Source Performance Standards

NSR New Source Review **NWA** National Wilderness Area **NWS** National Weather Service

 O_2 oxygen

PFCs perfluorocarbons

PFL Plant Fort Lauderdale the abbreviation for the FPL Lauderdale Plant

PM particulate matter

particulate matter less than 2.5 microns $PM_{2.5}$ PM₁₀ particulate matter less than 10 microns

ppb parts per billion

ppbvd parts per billion by volume dry

parts per million ppm

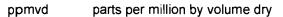
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PSD Prevention of Significant Deterioration

psia pound per square inch absolute psig pound per square inch gauge QA/QC quality assurance/quality control

RICE reciprocating internal combustion engines

SAM sulfuric acid mist

scf/yr standard cubic foot per year SCR selective catalytic reduction

SCRAM Support Center for Regulatory Air Models

SER significant emissions rate
SIL significant impact level
SF₆ sulfur hexafluoride
SO₂ sulfur dioxide
S.R. State Road
ST steam turbine

TPY

TSP total suspended particulate

TTN Technology Transfer Network

ULSD ultra low sulfur distillate "light oil"

tons per year

USGS U.S. Geological Survey

UTM Universal Transverse Mercator
VOC volatile organic compound
WCEC West County Energy Center







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INTRODUCTION

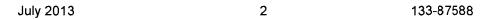
Florida Power & Light Company's (FPL's) existing Lauderdale Plant is located in Broward County Florida (see Figure 1-1) and includes two banks of 12 simple cycle gas turbines (GT1 through GT12 and GT13 through GT24). GT Units 1 through 12 began operation in August 1970, and the commercial in service dates for GT Units 13 through 24 was August 1972. Each bank of GTs has a nominal net capacity of 504 megawatts (MWs). GT Units 1 through 24 are authorized to operate pursuant to Florida Department of Environmental Protection (FDEP) Final Title V Permit No. 0110037-007-AV on natural gas and distillate oil.

In close proximity to the Lauderdale Plant is the Port Everglades Plant that includes one bank of similarly designed simple cycle GTs (GT1 through GT12) that are authorized to operate pursuant to FDEP Final Title V Permit No. 0110036-009-AV on natural gas and distillate oil. These 12 GTs also have a nominal net capacity of 504 MWs and have been operating since their commercial operation began in August 1971.

The existing 36 GTs located in Broward County are first generation gas turbine units that are used to serve peak and emergency demands in a quick start manner. Each unit consists of two aero-derivative gas turbines coupled with a single gas flow driven turbine-electric generator. These units have low stack heights (less than 50 feet) and relatively high nitrogen oxides (NO_x) emissions rates typical of these older generation units. NO_x emissions principally consist of nitrogen oxide (NO) and nitrogen dioxide (NO₂). The low stack heights in proximity to nearby property boundaries result in decreased dispersion properties and when combined with the relatively high NO_X emission rates result in elevated concentrations of NO2. A new 1-hour national ambient air quality standard (NAAQS) has been recently promulgated by EPA and adopted by FDEP that is much more stringent than the previous annual average NAAQS for NO2. Analyses of these 36 GT units found that the emissions from these units would not disperse sufficiently to bring off-site concentrations below the 1-hour NO2 NAAQS. FPL's evaluation concluded that the most cost effective solution is to replace the existing GTs with new, highly efficient combustion turbines with lower NO_x emission rates. FPL, after consultations and agreement with FDEP, understands that completing this project as expeditiously as possible is necessary to FDEP's implementation of the NAAQS Program and Section 172 of the Clean Air Act. Thus, FPL plans to bring five new CTs into service by December 31, 2016, that would assure 1-hour NO2 concentrations do not exceed the NAAQS at the property boundaries of the Lauderdale and Fort Myers plants.

This Air Construction Permit/Prevention of Significant Deterioration (PSD) Application consists of the retirement (except potentially two GTs to be retained for emergency black start capability only) of the existing Lauderdale GT Units (GT1 through GT24) and the Port Everglades GT Units (GT1 through GT12)







and replacement with five nominal 200 MW combustion turbines (CTs), effectively changing out the combustion technology of FPL's peaking resources to reduce emissions. These five CTs will be located at FPL's Lauderdale Plant and will be referred to as the Lauderdale CT Project ("Project"). The new CTs will be designated Units 6A through 6E.

Dismantlement of the existing generation units will occur after the new CTs are operational in order to maintain peak service capability in south Florida. There will be no overlap of operation between the existing GT units and new CTs.

There will be significant benefits associated with the Project. The five new CTs will be more energy efficient than the existing 36 GTs and will provide cleaner energy to FPL's customers. For the same amount of generation hourly, from 30 to 40 percent less fuel will be used in the new CT units compared to the older GT units. The maximum total air quality impacts for the Project are predicted to be well below and in compliance with the NAAQS. For pollutants such as NO₂, the Project's total air quality impacts are predicted to be significantly 40 percent or more lower than those predicted for the existing GTs.

In addition, air emission rates for NO_x with the Project will be approximately 90 percent lower than the existing GT emission rates, resulting in significantly lower air quality impacts.

The CTs being evaluated for the Project include the General Electric 7FA.05 and 7FA.04 CTs, and Siemens Power Generation, Inc. (Siemens) SGT6-5000F(5) CTs, or other vendor equivalents. The GE FA.05 CT has higher mass flow and produces more generation than the 7FA.04 CT. As a result, the emissions from GE FA.04 CT are enveloped by the GE FA.05 CT for the same emission rates (e.g., ppmvd; lb/MMBtu). Therefore, the GE 7FA.05 information was used for the analyses in this application. The information presented in this application envelops the performance and emissions for the above noted CTs being considered.

Each CT may utilize inlet air cooling and may consist of evaporative cooling or an alternative system. Evaporative cooling systems achieve adiabatic cooling using water in the form of water evaporated from a treated paper material. The evaporating water cools the inlet air stream when the water droplets are converted to water vapor. Inlet air temperature is reduced as heat is transferred at a rate of 1,075 British thermal units per pound (Btu/lb) of evaporated water. The result is a cooler, denser air stream. This allows additional power to be produced. The CTs will use natural gas and ultra low sulfur distillate (ULSD) oil as fuel. ULSD oil will be used for up to the equivalent of 500 hours per year (hr/yr) per CT at base load conditions.







Natural gas will be transported to the facility via existing pipeline. ULSD oil will be delivered to the facility by truck or pipeline and will be stored in two new ULSD oil storage tanks.

The U.S. Environmental Protection Agency's (EPA's) PSD regulations are promulgated under Title 40, Part 51.166 of the Code of Federal Regulations (40 CFR 51.166). Florida's PSD regulations are codified in FDEP Rule 62-212.400, Florida Administrative Code (F.A.C.), and have been approved by EPA. The Florida PSD regulations incorporate the requirements of EPA's PSD regulations. Under these requirements, the existing Lauderdale Plant is classified as an existing major facility. A modification to an existing major facility that results in a significant net emissions increase equal to or exceeding the significant emissions rates (SERs) listed in the Florida regulations under Section 62-212.400, Rule 62-212.400-2, F.A.C., is classified as a major modification and will be subject to the PSD preconstruction permitting program for those pollutants that exceed the PSD SERs.

The procedures for determining applicability of the PSD permitting program to the Project are specified in FDEP Rule 62-212.400(2), F.A.C. For each regulated pollutant, PSD is triggered as a result of a modification at an existing facility if the difference between the projected actual emissions and the baseline actual emissions equals or exceeds the SER for that pollutant, as defined at FDEP Rule 62-210.200 (243), F.A.C.

On June 3, 2010, EPA promulgated regulations related to PSD and Title V GHG Tailoring Rule [75 Federal Register (FR) 31514-31608]. This change in EPA's PSD regulations requires PSD review and approval for new major projects and modifications exceeding the PSD thresholds for review. This application includes information to address PSD review of GHGs under EPA's rules. Florida has deferred review and approval of projects undergoing PSD review for GHGs to EPA Region 4.

Using the required regulatory comparison of potential to baseline actual emissions when adding new emission units, there will be significant net increase in some regulated air emissions for the Project including GHGs. The net changes in air emissions, as presented in Section 2.0, will exceed the PSD SERs for many of the criteria pollutants subject to PSD review and GHGs. Therefore, pursuant to FDEP Rule 62-212.400, F.A.C., PSD review is applicable for the Project.

This Application is being filed for the purpose of obtaining an air construction/PSD permit for the Project in accordance with FDEP's federally approved major source air construction permit program under Florida's federally required State Implementation Plan. A separate application will be submitted to EPA Region 4 for PSD review and approval of GHG emissions. This Air Construction Permit Application Report is divided into seven major sections.







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- Section 1.0 presents an introduction to the Project
- Section 2.0 presents a description of the Project, including air emissions and stack parameters
- Section 3.0 provides a review of the regulatory analysis conducted, including PSD and nonattainment requirements, applicable to the Project
- Section 4.0 includes the control technology review including a Best Available Control Technology (BACT) analysis including GHG
- Section 5.0 discusses the ambient air monitoring analysis
- Section 6.0 presents a summary of the air modeling approach and results used in assessing compliance of the Project with NAAQS and PSD Increments.
- Section 7.0 presents the additional impact analysis required for PSD review.
- Appendices which include emission calculations, historical operation, BACT determinations and FDEP Form No. 62-210.900(1): Application for Air Permit Long Form.



2.0 PROJECT DESCRIPTION

2.1 Facility Description

The existing FPL Lauderdale Plant is located within the City of Dania Beach, in Broward County, Florida. The existing plant is situated within approximately 392 acres of land owned by FPL. The facility has access from Southwest 42nd Street and Griffin Road. Figure 2-1 presents the conceptual facility plot plan for the Project.

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2.2 New Combustion Turbines

The CTs (any of the models under consideration or equivalent) will use low- NO_x combustion technology or equivalent when firing natural gas and water injection when firing ULSD oil to minimize formation of NO_x . Natural gas and ULSD oil will be used as fuel. While FPL envisions that the new CTs will be operated as peaking and emergency capacity like the existing GTs, FPL is conservatively seeking permitting authority for maximum operation of 3,390 hr/yr (base load equivalent hours) for each CT of which ULSD oil usage is up to 500 hr/yr (base load equivalent hours) for each CT. This is an accepted operating assumption for permitting simple-cycle combustion turbine units in Florida.

The generating capacity of a CT is affected by ambient temperature, with increased temperature resulting in slightly less efficient electric production. Greater overall fuel consumption can occur at lower ambient temperatures. For the purpose of calculating maximum hourly fuel use quantities, the following specific operating conditions were used for the CTs (see Appendices A and B):

- 35 degrees Fahrenheit (°F) dry bulb turbine inlet temperature
- 60 percent relative humidity

The maximum heat input for the CTs being considered for the Project ranges from 1,754 MMBtu/hr, LHV (1,946 MMBtu/hr, HHV), to 2,022 MMBtu/hr, LHV (2,246 MMBtu/hr, HHV), when firing natural gas (100 percent capacity, 35°F). The corresponding maximum fuel usage ranges from about 2.2 million cubic feet per hour (MMcf/hr) to 1.9 MMcf/hr of natural gas for each CT. Maximum potential fuel usage at 75°F turbine inlet temperature ranges from about 2.9 × 10¹⁰ cubic feet per year (cf/yr) to 3.8 × 10¹⁰ cf/yr of natural gas for the Project operating 3,390 hours per year.

ULSD oil use will be based on the equivalent of 500 hr/yr per CT at full load. The maximum fuel use is about 16,500 gallons per hour per CT at 35°F turbine inlet with a maximum annual usage rate of 41 million gallons for five CTs each operating for 500 hours.





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Source Emission Units and Stack Parameters

The Project's air emission units are:

- 5 simple cycle CTs
- Black start generators (or retain two existing GTs for black start capability),
- Two 3 million gallon ULSD oil storage tanks.
- Fire water pump diesel engine

Each of these emission units is discussed in the following paragraphs.

Performance, estimated maximum hourly emissions, and exhaust information representative of each CT option operating at base load conditions (100 percent load) in simple cycle are presented in Tables 2-1a and 2-1b, and Tables 2-2a and 2-2b for natural gas and ULSD oil firing, respectively. Tables 2-1a and 2-1b and 2-2a and 2-2b are presented as versions "a" and "b", which are representative of the GE FA.05 and Siemens F5 CT models, respectively. The data are presented for a turbine inlet temperature of 75°F. The performance and emissions data for the other operating conditions are given in Appendices A and B for turbine inlet temperatures of 35°F, 75°F, and 95°F and various operating load conditions. Appendix A presents information on both the GE 7FA.05 and 7FA.04 models.

Maximum potential annual emissions for the CTs for regulated air pollutants using a turbine inlet temperature of 75°F. This turbine inlet temperature is conservative, since the annual average temperature is slightly higher than 75°F. To produce the maximum annual emissions, it is assumed that each CT would operate for 3,390 hours. Of the 3,390 operating hours, an average of 2,890 hr/yr is assumed to be natural gas firing (except for maximum emissions of SO₂). For the remaining average of 500 hr/yr, the CTs are assumed to operate on ULSD oil.

Since the ULSD (0.0015 percent) oil has lower fuel sulfur content than that assumed for natural gas (2 gr/100 scf), the maximum annual SO₂ and sulfuric acid mist (SAM) emissions are based on 3,390 hours of operation firing natural gas. Tables 2-3a and 2-3b present the maximum potential annual emissions for the range of operating conditions for each CT being considered for the Project.

A process flow diagram of the new CT configuration, operating at base load conditions with a compressor inlet temperature of 75°F, is presented in Figure 2-2.

During combustion, two primary types of NO_x are formed: fuel NO_x and thermal NO_x. Fuel NO_x emissions are formed through the oxidation of a portion of the nitrogen contained in the fuel. Thermal NO_x emissions are generated through the oxidation of a portion of the nitrogen contained in the combustion







air. NO_x formation can be limited by lowering combustion temperatures (through water injection) and/or staging combustion (a reducing atmosphere followed by an oxidizing atmosphere). Emissions of NO_x for the CTs are proposed at concentrations of 9 parts per million by volume dry (ppmvd) conditions, corrected to 15 percent oxygen (O_2) when firing natural gas and 42 ppmvd corrected to 15 percent O_2 when firing ULSD oil.

Carbon monoxide (CO) is formed by incomplete combustion of fuel. High combustion temperatures, adequate excess air, and good fuel/air mixing during combustion will minimize CO formation. CO formation is limited by ensuring complete efficient combustion of the fuel in the turbines. Recent improvements in CT combustor technology allow for both reduced NO_x emissions and low CO emissions.

The expected CO stack emission rates at base load for the GE CTs or equivalent when firing natural gas are 9 ppmvd operation and 20 ppmvd with ULSD oil firing. For the Siemens CTs, the expected CO emission rates at base load when firing natural gas are 4 ppmvd corrected to 15 percent O₂ when firing gas, and 9 ppmvd corrected to 15 percent O₂ with ULSD oil firing.

Similarly, volatile organic compound (VOC) emissions are formed by incomplete combustion of fuel. High combustion temperatures, adequate excess air, and good fuel/air mixing during combustion will minimize VOC formation. VOC formation is limited by ensuring complete efficient combustion of the fuel in the CTs. Recent improvements in CT combustor technology allow for both reduced NO_x emissions and low VOC emissions.

The expected VOC emission rates for the GE CTs or equivalent at base load operation when firing natural gas are 1.4 ppmvd corrected to 15 percent O_2 at base load operation and 3.5 ppmvd corrected to 15 percent O_2 for ULSD oil firing. For the Siemens CTs or equivalent at base load operation, the expected VOC emission rates when firing natural gas are 1.0 ppmvd corrected to 15 percent O_2 at base load operation and 1.0 ppmvd corrected to 15 percent O_2 for ULSD oil firing.

SO₂ emission rates are controlled and minimized by the very low sulfur content in the fuels, which will be a maximum of 2 gr/100 scf sulfur for natural gas and 0.0015 percent sulfur by weight for ULSD oil.

The Project may be equipped with four nominal 3,000 kilowatt (kW) emergency generators firing ULSD oil for black start capability. These emergency generators will be used when electric power is not available to start the CTs. This primarily would occur during catastrophic events such as hurricanes. Table 2-4 contains representation performance and emissions information for the black start diesel generators proposed for the Project, based on 100 hr/yr operation for permitting purposes. Normally these







emergency generators would be operated 1 to 2 hours per month for maintenance and reliability testing. Alternatively, two of the 24 existing gas turbines may be kept to provide this black start capability.

The Project will be equipped with a 300 horsepower (hp) fire pump engine using ULSD oil. This engine will be used when necessary during catastrophic events such as fires. Table 2-4 presents typical emissions and manufacturer's information for the fire pump engine, based on 100 hr/yr operation for permitting purposes. The fire pump engine will typically be operated only 1 to 2 hours per month for maintenance and reliability testing.

ULSD oil will be either trucked or piped to the facility and stored in two new ULSD oil tanks at the facility. Each tank is a vertical fixed roof design, with a rated storage capacity of approximately 3.0 million gallons (about 70,000 barrels). Appendix A provides emissions information for the ULSD oil storage tanks.

2.4 Annual Emissions for the Project

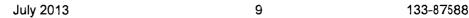
The maximum annual potential emissions for the Project include air emissions from the CT, emergency generators, and ULSD oil storage tanks. Tables 2-5a and 2-5b present the maximum annual potential emissions with the GE and Siemens CTs, respectively. These tables address the criteria pollutants, as required, under new source review.

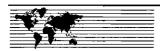
In addition, maximum annual potential hazardous air pollutants (HAPs) emissions are presented in Tables 2-6a and 2-6b for GE 7FA.05 and Siemens F5 CT models, respectively. Additional detail on the HAP emission calculations is also presented in Appendices A and B. The Lauderdale Plant will continue to be a major source of hazardous air pollutant (HAP) emissions due to the combined potential emissions from the Project and existing combined cycle unit exceed the major source for HAPs [10 tons per year (TPY) of a single HAP, or 25 TPY for all HAPs].

Annual emissions were based on maximum emissions for base load operation and ambient temperatures of 75°F. The maximum emissions of all regulated air pollutants except SO₂ are based on 2,890 hr/yr firing natural gas and 500 hr/yr firing oil. The maximum SO₂ emissions are based on natural gas firing for 3,390 hr/yr. The potential emissions are based 100 percent load condition at a turbine inlet temperature of 75°F, since this temperature represents a conservative annual average temperature for the area.

Tables 2-5a and 2-5b compare the net emission changes due to the Project, reflecting the maximum Project emissions as well as the emission reductions from retirement of the existing GT Units 1 through 24, to the PSD SERs. The PSD SERs are the emission thresholds to determine if PSD review will be required for modifications to major sources. The historical actual emissions for the existing GT Units 1







through 24 that are presented in these tables were determined pursuant to FDEP PSD Rules, specifically FDEP Rule 62-212.400 (2)(a)1., F.A.C. Five years (2008 through 2012) of historical emission data were evaluated to determine historical actual emissions using the highest 2 year average emissions for each pollutant. Historical actual emissions are based on past Annual Operating Reports (AORs), which are presented in a series of tables in Appendix C for each unit for each year. In Tables 2-5a and 2-5b, the net emission changes (i.e., projected maximum potential emissions minus historical actual emissions) are compared to the PSD SERs. If the PSD SER for a pollutant is not exceeded by this comparison, PSD review is not required for that pollutant.

As shown in these tables, there are significant net emission increases for most pollutants. Therefore, PSD review is required for particulate matter (PM), particulate matter less than 10 microns (PM₁₀), particulate matter less than 2.5 microns (PM_{2.5}), and NO_x, CO, VOCs and GHG.

2.5 Annual Emissions for GHGs

On June 3, 2010, EPA promulgated regulations related to Prevention of Significant Deterioration and Title V Greenhouse Gas Tailoring Rule (75 FR 31514-31608). In EPA's promulgation, GHGs are defined to include an aggregate group of six GHGs: CO₂, methane (CH₄), nitrous oxide (N₂O), hydrofluorocarbons (HFCs), perfluorocarbons (PFCs), and sulfur hexafluoride (SF₆). Each of these GHGs has a specific Global Warming Potential that is calculated as "CO₂ equivalent emissions" or CO₂e that is equivalent to one ton of CO₂.

For the Project, the GHGs emitted are CO_2 , CH_4 , and N_2O with one ton of CH_4 equivalent to 21 tons of CO_2e and one ton of N_2O equivalent to 310 tons of CO_2e . Tables 2-5a to 2-5b present the net emission changes resulting from the Project, reflecting the maximum projected the Project emissions and the resulting changes compared to the existing GT Units 1 through 24 and the PSD SERs, which are thresholds for PSD review for modifications to major sources.

GHGs were calculated based on the actual annual heat input and emission factors from 40 CFR 98, Subpart C. These GHG emissions show the CO₂e rates for these pollutants. PSD review is required for GHG emissions greater than the listed PSD SER of 75,000 tons CO₂e. For PSD applicability purposes, Tables 2-5a and 2-5b, show the maximum potential emission of GHGs will exceed the baseline actual emissions of GT Units 1 through 24, primarily due to greater assumed operation than the existing GTs. A separate application will be submitted to EPA Region 4 for PSD review and approval of GHG emissions.









2.6 Layout, Structures, and Stack Sampling Facilities

A conceptual facility plot plan of the Project is presented in Figure 2-1. Typical dimensions of the structures associated with the CTs are presented in Section 6.0. Stack sampling facilities will be constructed in accordance with FDEP Rule 62-297.310(6), F.A.C.

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2.7 Excess Emissions

In addition to the excess emissions allowed pursuant to FDEP Rule 62-210.700, F.A.C., a provision for Combustion and Full Speed No Load (FSNL) tuning similar to that authorized for other CT in FPL's fleet is requested. The proposed condition follows:

Combustion Tuning / FSNL Testing: Continuous monitoring data collected during initial or other major combustion tuning sessions and during manufacturer required Full Speed No Load (FSNL) operations shall be excluded from the continuous monitoring compliance demonstration provided the tuning session is performed in accordance with the manufacturer's specifications. A "major tuning session" would occur after a combustor change-out, a major repair or maintenance to a combustor, or other similar circumstances. Prior to performing any major tuning session, the permittee shall provide the Compliance Authority with an advance notice of at least one working (business) day that details the activity and proposed tuning schedule. The notice may be by telephone, facsimile transmittal, or electronic mail. (from West County Energy Center Title V Facility 0990646)





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3.0 AIR QUALITY REVIEW REQUIREMENTS AND APPLICABILITY

The following discussion pertains to federal, state, and local air regulatory requirements and their applicability to the Project.

3.1 National, State, and Local AAQS

The existing applicable national and Florida AAQS are presented in Table 3-1. Primary NAAQS were promulgated to protect the public health with an adequate margin of safety and secondary NAAQS were promulgated to protect the public welfare from any known or anticipated adverse effects associated with the presence of pollutants in the ambient air. Areas of the country in compliance with NAAQS are designated as attainment areas. New sources to be located or modified sources located in or near these areas may be subject to more stringent air permitting requirements.

3.2 PSD Requirements

3.2.1 General Requirements

Under federally approved Florida PSD review requirements, all major new or modified sources of air pollutants regulated under the Clean Air Act (CAA) must be reviewed and a pre-construction permit issued.

PSD is applicable to a "major facility" and certain "modifications" that occur at a major facility. A major facility is defined as any 1 of 28 named source categories that have the potential to emit 100 TPY or more, or any other stationary facility that has the potential to emit 250 TPY or more, of any pollutant regulated under the CAA. "Potential to emit" means the capability, at maximum design capacity, to emit a pollutant after the application of control equipment. Net emission increases from a modification at a major facility that exceed the PSD SERs are also subject to PSD review.

EPA has promulgated regulations providing that certain increases above an air quality baseline concentration level of SO₂, PM₁₀, and NO₂ concentrations that would constitute significant deterioration. The EPA class designations and allowable PSD increments are presented in Table 3-1. Florida has adopted the EPA class designations and allowable PSD increments for SO₂, PM₁₀, and NO₂.

PSD review is used to determine whether significant air quality deterioration will result from the new or modified facility. Florida's PSD regulations are found in FDEP Rule 62-212.400, F.A.C. Major new facilities and major modifications are required to undergo the following analysis related to PSD for each pollutant emitted in significant amounts (see Table 3-2):







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- 1. Control technology review,
- 2. Source impact analysis,
- 3. Air quality analysis (monitoring),
- 4. Source information, and
- 5. Additional impact analyses.

In addition to these analyses, a new major facility or major modification made to an existing major facility also must be reviewed with respect to Good Engineering Practice (GEP) stack height regulations. Discussions concerning each of these requirements for a new major facility or major modification are presented in the following sections.

3.2.2 Greenhouse Gases

On June 3, 2010, EPA issued a "Tailoring Rule" that "tailors" the applicability provisions of the PSD and Title V programs to enable EPA and state agencies to phase in permitting requirements for GHGs. The first phase of the Tailoring Rule began on January 2, 2011, and continued through June 30, 2011. During this period GHG sources became subject to PSD if the increase in GHG emissions from a project exceeded 75,000 TPY of CO₂e or more and the project was required to undergo PSD review for other air regulated pollutants. The second phase of the Tailoring Rule began on July 1, 2011, and continues thereafter for new major GHG emitting facilities and major modifications. New major sources with the potential to emit 100,000 TPY CO₂e or more of GHG will be considered major sources for PSD permitting purposes and are required to undergo PSD review. Additionally, any physical change or change in the method of operation at a major source resulting in a net GHG emissions increase of 75,000 TPY CO₂e or more will be subject to PSD review.

For PSD purposes, GHGs are a single air pollutant defined as the aggregate group of the following six gases: CO₂, N₂O, CH₄, HFCs, PFCs, and SF₆.

Once major sources become subject to PSD, these sources must meet the various PSD requirements in order to obtain a PSD permit. However, there are no ambient air quality standards or PSD increments for GHGs. Therefore, the requirements for a source impact analysis, air quality analysis (monitoring), and additional impact analyses are not required. PSD review for GHGs principally involves the control technology review that includes a determination of BACT. The EPA published the PSD and Title V permitting guidance for GHGs in March 2011 that provides guidance on BACT analyses for GHG emissions.





3.2.3 Control Technology Review

A new major facility or major modification must perform a control technology review, which requires that all applicable federal and state emission limiting standards be met and that BACT be applied to control emissions from the source (FDEP Rule 62-212.400, F.A.C.). The BACT requirements are applicable to all regulated pollutants for which the increase in emissions from the facility or modification exceeds the SER (see Table 3-2).

BACT is defined in FDEP Rule 62-210.200(40), F.A.C., as:

- (a) An emission limitation, including a visible emissions standard, based on the maximum degree of reduction of each pollutant emitted, which the Department, on a case-by-case basis, determines is achievable through application of production processes and available methods, systems and techniques (including fuel cleaning or treatment or innovative fuel combustion techniques) for control of each such pollutant taking into account:
 - 1. Energy, environmental and economic impacts, and other costs,
 - 2. All scientific, engineering, and technical material and other information available to the Department, and
 - 3. The emission limiting standards or BACT determinations of Florida and any other State.
- (b) If the Department determines that technological or economic limitations on the application of measurement methodology to a particular part of an emissions unit or facility would make the imposition of an emission standard infeasible, a design, equipment, work practice, operational standard or combination thereof, may be prescribed instead to satisfy the requirement for the application of BACT. Such standard shall, to the degree possible, set forth the emissions reductions achievable by implementation of such design, equipment, work practice or operation.
- (c) Each BACT determination shall include applicable test methods or shall provide for determining compliance with the standard(s) by means which achieve equivalent results.
- (d) In no event shall application of best available control technology result in emissions of any pollutant which would exceed the emissions allowed by any applicable standard under 40 CFR Parts 60, 61, and 63.

The BACT requirements are intended to ensure that the control systems incorporated in the design of a new facility reflect the latest in control technologies used in a particular industry and take into consideration existing and future air quality in the vicinity of the new facility. BACT must, at a minimum, demonstrate compliance with NSPS for a source (if applicable). An evaluation of the air pollution control techniques and systems, including a cost-benefit analysis of alternative control technologies capable of achieving a higher degree of emission reduction than the proposed control technology, is required. The cost-benefit analysis requires the documentation of the materials, energy, and economic penalties associated with the proposed and alternative control systems, as well as the environmental benefits







derived from these systems. A decision on BACT is to be based on sound judgment, balancing environmental benefits with energy, economic, and other impacts (EPA, 1978).

For GHG emissions, control technology review is conducted by EPA under its regulations in 40 CFR 52.21. EPA issued guidance on the determination of BACT for GHGs ("PSD and Title V Permitting Guidance for Greenhouse Gases", March 2011). This EPA guidance supplements previous EPA guidance on the determination of BACT that is specific to BACT determinations for GHG emissions.

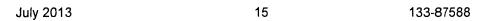
3.2.4 Source Impact Analysis

A source impact analysis must be performed for a new major facility or major modification to a major source for each pollutant, subject to PSD review, for which net emissions exceed the SER (Table 3-2). The PSD regulations specifically provide for the use of atmospheric dispersion models in performing impact analyses, estimating baseline and future air quality levels, and determining compliance with NAAQS and allowable PSD increments. Designated EPA models that are approved by FDEP normally must be used in performing the impact analysis. Specific applications for other than EPA approved models require EPA's consultation and prior approval. Guidance for the use and application of dispersion models is presented in the EPA publication *Guideline on Air Quality Models (Revised)*. The source impact analysis for criteria pollutants to address compliance with NAAQS and PSD Class II increments may be limited to the new source if the impacts as a result of the new source are below significant impact levels, as presented in Table 3-1.

The EPA has proposed significant impact levels for Class I areas. Although these levels have not been officially promulgated as part of the federal PSD regulations and may not be binding for states in performing PSD reviews, the levels serve as a guideline in assessing a source's impact in a Class I area. FDEP has accepted the use of these significant impact levels.

Various lengths of meteorological data records can be used for impact analysis. A 5 year period can be used with corresponding evaluation of highest, second highest short term concentrations for comparison to NAAQS or PSD increments. The term "highest, second highest" (HSH) refers to the highest of the second highest concentrations at all receptors (i.e., the highest concentration at each receptor is discarded). The second highest concentration is significant because short term NAAQS specify that the standard should not be exceeded at any location more than once a year. If fewer than 5 years of meteorological data are used in the modeling analysis, the highest concentration at each receptor normally must be used for comparison to air quality standards.







Because there are no NAAQS or PSD increments applicable to GHG emissions, these analyses are not conducted for PSD review for GHG.

3.2.5 Air Quality Monitoring Requirements

In accordance with requirements of FDEP Rule 62-212.400(5)(f), F.A.C., PSD review for a new major facility or major modification must consider an analysis of continuous ambient air quality data in the area affected by the proposed major PSD source or major modification. For a new major facility or major modification, the affected pollutants are those that the facility potentially would emit above the SERs.

Ambient air monitoring for a period of up to 1 year generally is appropriate to satisfy the PSD monitoring requirements. Data for a minimum of 4 months are required. Existing data from the vicinity of the proposed source may be used, if the data meet certain quality assurance requirements; otherwise, additional data may need to be gathered. Guidance in designing a PSD monitoring network is provided in *Ambient Monitoring Guidelines for Prevention of Significant Deterioration* (EPA, 1987a).

The regulations include an exemption that excludes or limits the pollutants for which an air quality analysis must be conducted. This exemption states that a proposed major stationary facility is exempt from the monitoring requirements with respect to a particular pollutant, if the emissions of the pollutant from the facility would cause, in any area, air quality impacts less than the *de minimis* levels presented in Table 3-2 (FDEP Rule 62-212.400-3, F.A.C.). If a facility's predicted impacts are less than the *de minimis* levels, then preconstruction monitoring is not required.

Because there are no ambient monitoring methods applicable to GHG emissions, these analyses are not conducted for PSD review for GHG.

3.2.6 Source Information/GEP Stack Height

Source information must be provided to adequately describe the proposed facility or major modification subject to PSD review.

The 1977 CAA Amendments require that the degree of emission limitation required for control of any pollutant cannot be affected by a stack height that exceeds GEP or any other dispersion technique. On July 8, 1985, EPA promulgated final stack height regulations (EPA, 1985a). Identical regulations have been adopted by FDEP (FDEP Rule 62-210.550, F.A.C.). GEP stack height is defined as the highest of:

- 1. 65 meters; or
- 2. A height established by applying the formula:

Hg = H + 1.5 L





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where:

Hg = GEP stack height,

H = Height of the structure or nearby structure, and

L = Lesser dimension (height or projected width) of nearby structure(s); or

3. A height demonstrated by a fluid model or field study.

"Nearby" is defined as a distance up to 5 times the lesser of the height or width dimensions of a structure or terrain feature, but not greater than 0.8 kilometer (km). Although GEP stack height regulations require that the stack height used in modeling for determining compliance with NAAQS and PSD increments not exceed the GEP stack height, the actual stack height may be greater.

The stack height regulations also allow increased GEP stack height beyond that resulting from the above formula in cases where plume impaction occurs. Plume impaction is defined as concentrations measured or predicted to occur when the plume interacts with elevated terrain. Elevated terrain is defined as terrain that exceeds the height calculated by the GEP stack height formula.

3.2.7 Additional Impact Analysis

In addition to air quality impact analyses, Florida PSD regulations require analyses for applicable pollutants of the impairment to visibility and the impacts on soils and vegetation that would occur as a result of a new major facility or major modification subject to PSD review [FDEP Rule 62-212.400(5)(e), F.A.C.]. Impacts as a result of general commercial, residential, industrial, and other growth associated with the source also must be addressed. These analyses are required for each pollutant emitted in significant amounts (see Table 3-2).

Because GHG emissions will not cause visibility impairment or direct impacts to soils and vegetation, these analyses are not conducted for PSD review for GHG.

3.2.8 Air Quality Related Values

An Air Quality Related Value (AQRV) analysis is required for projects for those pollutants undergoing PSD review to assess the potential impact on AQRVs in PSD Class I areas. The nearest Class I areas to the Project are the Everglades National Park (ENP), located about 48 km (29 miles) from the Project, and the Chassahowitzka National Wilderness Area (NWA), located more than 300 km (180 miles) from the Project. The U.S. Department of the Interior in 1978 administratively defined AQRVs to be:

All those values possessed by an area except those that are not affected by changes in air quality and include all those assets of an area whose vitality, significance, or integrity is dependent in some way upon the air environment. These values include visibility and







those scenic, cultural, biological, and recreational resources of an area that are affected by air quality.

Important attributes of an area are those values or assets that make an area significant as a national monument, preserve, or primitive area. They are the assets that are to be preserved if the area is to achieve the purposes for which it was set aside (Federal Register, 1978).

The AQRVs include visibility, freshwater and coastal wetlands, dominant plant communities, unique and rare plant communities, soils and associated periphyton, and the wildlife dependent on these communities for habitat. Rare, endemic, threatened, and endangered species of the NP and bioindicators of air pollution (e.g., lichens) must also be evaluated.

3.3 Nonattainment Rules

FDEP has nonattainment provisions (FDEP Rule 62-212.500, F.A.C.) that apply to all new major facilities or major modifications to major facilities located in a nonattainment area. In addition, for these facilities that are located in an attainment or unclassifiable area, the nonattainment review procedures apply if the source or modification is located within the area of influence of a nonattainment area. The Project is located in Broward County, which is classified as an attainment area for all criteria pollutants. Therefore, nonattainment New Source Review (NSR) requirements are not applicable.

3.4 Emission Standards

3.4.1 New Source Performance Standards

The NSPS are a set of national emission standards that apply to specific categories of new sources. As stated in the 1977 CAA Amendments, these standards "shall reflect the degree of emission limitation and the percentage reduction achievable through application of the best technological system of continuous emission reduction the Administrator determines has been adequately demonstrated."

The Project will be subject to one or more NSPS. EPA promulgated new NSPS for Stationary Combustion Turbines that will commence construction after February 18, 2005. Subpart KKKK replaces Subpart GG for CTs. On October 15, 2003, EPA promulgated changes to 40 CFR 60, Subpart Kb that would exempt ULSD oil tanks containing No. 2 ULSD oil by virtue of its vapor pressure (FR Vol. 68, No. 199, Pages 59328-59333).

Combustion Turbine

 NO_x and SO_2 emissions from all stationary CTs with a heat input at peak load equal to 10.7 gigajoules per hour (10 MMBtu/hr), based on the lower heating value of the fuel fired, are limited per 40 CFR 60 Subpart KKKK. NO_x emissions for these new CTs (i.e., >850 MMBtu/hr) are limited by Subpart KKKK to







15 ppmvd corrected to 15 percent O_2 and 42 ppmvd corrected to 15 percent O_2 for natural gas and oil firing, respectively. SO_2 emissions are limited to using a fuel with a sulfur content of no greater than 0.05 percent and 20 gr/10 scf of sulfur for oil and natural gas firing, respectively. In addition to emission limitations, there are requirements for performance testing and monitoring in 40 CFR 60 Subpart KKKK.

There are also applicable notification, reporting, and recordkeeping requirements in the general provisions of 40 CFR 60 Subpart A. These are summarized below:

40 CFR 60.7 Notification and Record Keeping

- (a)(1) Notification of the date of construction 30 days after such date.
- (a)(3) Notification of actual date of initial startup within 15 days after such date.
- (a)(5) Notification of date which demonstrates CEM not less than 30 days prior to date 60.7 (b) Maintain records of all startups, shutdowns, and malfunctions.
 - (c) Excess emissions reports semi-annually by the 30th day following 6-month period (required even if no excess emissions occur).
 - (d) Maintain file of all measurements for 2 years.

60.8 Performance Tests

- (a) Must be performed within 60 days after achieving maximum production rate, but no later than 180 days after initial startup.
- (d) Notification of Performance tests at least 30 days prior to them occurring.

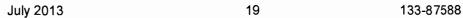
Other Emission Units

NSPS are also applicable to the black start generators. For the project the black start diesel generators meet the definition of "emergency stationary internal combustion engine" in NSPS Subpart IIII, Standards of Performance for Stationary Compression Ignition Internal Combustion Engines. This NSPS is applicable and the black start generators would be operated for according to Section 60.4211(f).

3.4.2 National Emission Standards for Hazardous Air Pollutants

EPA has promulgated maximum achievable control technology (MACT) standards under the National Emissions Standards for Hazardous Air Pollutants (NESHAPs) regulations. Maximum annual potential HAPs emissions were presented in Tables 2-6a and 2-6b for the GE 7FA.05 CTs and Siemens "F5" CTs, respectively. Additional detail on the HAP emission calculations is also presented in Appendices A and B.







The Lauderdale Plant remains a major source of HAPs due to the combined emissions of Units 4 and 5 and the potential emissions associated with the Project. Therefore, certain MACT standards under the NESHAP regulations would apply. Under the NESHAPs of 40 CFR Part 63, Subpart YYYY applies to the CTs and Subpart ZZZZ applies to the reciprocating internal combustion engines (RICE). For the later, meeting the requirements of NSPS Subpart IIII meets the requirements of NESHAP Subpart ZZZZ.

3.4.3 Florida Rules

FDEP has adopted the EPA NSPS by reference in FDEP Rule 62-204.800(7): Subsection (b)39 for stationary gas turbines and Subsection (b)16 for volatile organic liquid storage vessels. Therefore, the facility is required to meet the same emissions, performance testing, monitoring, reporting, and record keeping as those described in Section 3.4.1. FDEP has authority for implementing NSPS requirements in Florida.

3.4.4 Florida Air Permitting Requirements

The FDEP regulations require any new source to obtain an air permit prior to construction. Major new sources must meet the appropriate PSD and nonattainment requirements as discussed previously. Required permits and approvals for air pollution sources include NSR for nonattainment areas, PSD, NSPS, NESHAP, Permit to Construct, and Permit to Operate. The requirements for construction permits and approvals are contained in FDEP Rules 62-4.030, 62-4.050, 62-4.210, 62-210.300(1), and 62-212.400, F.A.C. Specific emission standards are set forth in Chapter 62-296, F.A.C.

This Application is being filed for the purpose of establishing federally enforceable emission limitations that ensure the Project will not result in a significant net increase in emissions of any regulated air pollutant, in accordance with FDEP's federally approved minor source air construction permit program under Florida's federally approved SIP.

3.4.5 Local Air Regulations

The Pollution Prevention, Remediation and Air Quality Division (PPRAQD) of Broward County Environmental Protection and Growth Management Department is the air compliance authority for the County, implementing FDEP regulations. PPRAQD has been delegated authority to review, process, and take appropriate action (i.e., exempt, issue, or deny) on most FDEP District-Level permits within the County. However, permits for electrical power plants are issued by FDEP, and PPRAQD provides review of the application during FDEP's review period.





3.5 Source Applicability

3.5.1 Area Classification

The Project is located in Broward County, which has been designated by EPA and FDEP as an attainment area (includes unclassifiable) for all criteria pollutants. Broward County and surrounding counties are designated as PSD Class II areas for SO₂, PM [total suspended particulate (TSP)], and NO₂. The nearest Class I area to Project is the ENP, located approximately 48 km (29 miles) from the Project, and Chassahowitzka NWA, located more than 300 km (180 miles) from the Project.

3.5.2 PSD Review

Pollutant Applicability

The FPL Lauderdale Plant is considered to be a major facility under FDEP PSD rules because the emissions of several regulated pollutants are will exceed 100 TPY and the emissions units are one of the 28 listed major source categories under the PSD rules. The Project is defined as a major modification under the PSD rules and PSD review is required for any pollutant for any PSD-regulated air emissions that exceed the PSD significant emission rates. As shown in Table 3-3, potential emissions from the proposed Project will trigger PSD review for PM (TSP), PM₁₀, PM_{2.5}, NO_x, CO, and VOC. (Note: EPA no longer requires PSD review for HAPs from PSD review. The pollutants vinyl chloride, asbestos, and beryllium are no longer evaluated in PSD review because they are addressed through the NESHAP program.)

Emission Standards

 NO_x and SO_2 emissions from all stationary CTs with a heat input at peak load equal to 10.7 gigajoules per hour (10 MMBtu/hr), based on the lower heating value of the fuel fired, are limited per 40 CFR 60 Subpart KKKK adopted by reference by FDEP in Rule 62-204.800(8)(b)78 F.A.C.. NO_x emissions for these new CTs (i.e., >850 MMBtu/hr) are limited by Subpart KKKK to 15 ppmvd corrected to 15 percent O_2 and 42 ppmvd corrected to 15 percent O_2 for natural gas and oil firing, respectively. SO_2 emissions are limited to using a fuel with a sulfur content of no greater than 0.05 percent and 20 gr/100 scf of sulfur for oil and natural gas firing, respectively. These requirements are summarized in Section 4.2. In addition to emission limitations, there are requirements for performance testing and monitoring in 40 CFR 60 Subpart KKKK. There are also applicable notification, reporting, and recordkeeping requirements in the general provisions of 40 CFR 60 Subpart A. The proposed emissions for CTs being considered for the Project will be well below the specified limits (see Section 4.0).

EPA has promulgated MACT standards under the NESHAP regulations and applicability is based on whether a source is major or minor for HAPs. A facility is classified as a major source of HAPs when the maximum potential emissions for all emission units located at the facility exceed 10 TPY of a single HAP







and 25 TPY for all HAPs. The Lauderdale Plant will remain a major source of HAPs due to the combined potential emissions of the Project along with the existing combustion turbines associated with Units 4 and 5.

The NESHAP Subpart YYYY applies to the CTs being considered if the aggregate use of oil by existing and new turbines exceeds 1,000 hours during any calendar year. However, information available from the equipment vendors indicate that the CTs being considered will meet the proposed MACT of 91 parts per billion by volume dry (ppbvd) corrected to 15 percent O₂ for formaldehyde. FDEP adopted this EPA rule by reference in Rule 62-204.800(11)(b)81 F.A.C.

The NESHAP Subpart ZZZZ addressing RICE applies to both major and area sources of HAPs. FDEP adopted this EPA rule by reference in Rule 62-204.800(11)(b)82, F.A.C. The method of compliance under this rule is demonstrating compliance with 40 CFR 60, Subpart IIII, which was previously cited in this section. The emergency generators and fire pump engine will meet the requirements of Subpart IIII.

Ambient Monitoring

For the Project, the impacts will be less than the PSD de minimis monitoring concentrations for certain pollutants (see Section 5.0). As a result, an air quality monitoring impact analysis for these pollutants is not required by NSR under FDEP air regulations. For O₃ and PM_{2.5}, air quality monitoring data are provided, which demonstrate that Broward County is in attainment of NAAQS for these pollutants. These data are presented in Section 5.0 of this application.

GEP Stack Height Impact Analysis

The GEP stack height regulations allow any stack to be at least 65 meters (213 ft) high. The CT stacks will be 80 ft. These stack heights do not exceed the GEP stack height. However, as discussed in Section 6.0, Air Quality Modeling Approach, since the stack height is less than GEP, building downwash effects must be considered in the modeling analysis. As a result, the potential for downwash of the CT emissions caused by nearby structures is included in the modeling analysis.

3.5.3 Local Air Regulations

As specified in Subsection 3.4.5, PPRAQD does not have delegated authority to review, process, or take appropriate action over electrical power plant projects; therefore, permitting requirements for the Project will comply with FDEP permitting requirements.





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3.5.4 Other Clean Air Act Requirements

The 1990 CAA Amendments established a program to reduce potential precursors of acidic deposition. The Acid Rain Program was delineated in Title IV of the CAA Amendments and required EPA to develop the program. EPA's final regulations were promulgated on January 11, 1993, and included permit provisions (40 CFR 72), allowance system (Part 73), continuous emission monitoring (CEM) (Part 75), excess emission procedures (Part 77), and appeal procedures (Part 78). FDEP adopted these rules by reference in Rule 62-204.800(16) F.A.C. (permit provisions), Rule 62-204.800(17) F.A.C. (allowance system), Rule 62-204.800(19) F.A.C.[continuous emission monitoring (CEM)], Rule 62-204.800(21) F.A.C. (excess emission procedures), and Rule 62-204.800(22) F.A.C. (appeal procedures).

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EPA's Acid Rain Program applies to all existing and new utility units, except those serving a generator less than 25 MW, existing simple cycle CTs, and certain non-utility facilities; units which fall under the program are referred to as affected units. The EPA regulations are applicable to the Project for the purposes for obtaining a permit and allowances, as well as emission monitoring. New units are required to obtain permits under the program by submitting a complete application 24 months before the date on which the unit commences operation (e.g., first fire).

The permit would require the units to hold SO₂ emission allowances. Emission limitations established in the Acid Rain Program are presumed to be less stringent than BACT for new units. An allowance is a market based financial instrument that is equivalent to 1 ton of SO₂ emissions. Allowances can be sold, purchased, or traded.

NO_x monitoring is required for natural gas-fired and oil-fired affected units using CEM or alternate procedures. SO₂ monitoring is also required, although use of CEM is optional. When an SO₂ CEM system is selected to monitor SO₂ mass emissions, a flow monitor is also required. Alternately, SO₂ emissions may be determined using procedures established in Appendix D, 40 CFR 75 (FDEP Rule 62-204.800(19)(b)4 F.A.C.; flow proportional oil sampling or manual daily oil sampling). CO₂ emissions must also be determined either through a CEM (e.g., as a diluent for NO_x monitoring) or calculation. Alternate procedures, test methods, and quality assurance/quality control (QA/QC) procedures for CEM are specified (Part 75, Appendices A through I; FDEP Rule 62-204.800(19)(b)1-9 F.A.C.). The acid rain CEM requirements including QA/QC procedures are, in general, more stringent than those specified in the NSPS for Subpart KKKK. New units are required to meet the requirements by not later than 90 days after the unit commences commercial operation.





4.0 CONTROL TECHNOLOGY DESCRIPTION

4.1 Introduction

4.1.1 Applicability and BACT Approach

The PSD regulations require new major stationary sources or major modifications to existing major sources to undergo a control technology review for each pollutant that may potentially be emitted above significant amounts. As discussed in previous sections, PSD review is required for the Project.

There are NSPS regulations which are applicable to emissions of NO_x and SO₂ from the CTs. NSPS are also applicable to the black-start generators and fire pump engine. For the project, the black start diesel generators and fire pump engine meet the definition of "emergency stationary internal combustion engine" in NSPS Subpart IIII, Standards of Performance for Stationary Compression Ignition Internal Combustion Engines. The Clean Air Act specifies that BACT cannot be less stringent than any applicable standard of performance under the NSPS standards, which were discussed in Section 3.5.2. Subsection 4.2 presents the BACT analysis for non-GHG pollutants including NO_x, CO, VOCs and PM/PM₁₀/PM_{2.5}.

The approach to the BACT analysis is based on the regulatory definitions of BACT, as well as consideration of EPA's current guidelines suggesting that a "top-down" approach be followed in BACT analyses. The CAA and corresponding implementing regulations require that a BACT analysis be conducted on a case by case basis taking into consideration the amount of emissions reductions that each available emissions reducing technology or technique would achieve, as well as the energy, environmental, economic and other costs associated with each technology or technique.

EPA has recommended since 1990 that permitting authorities use the five step "top down" BACT process to determine BACT. The top down process calls for all available control technologies for a given pollutant to be identified and ranked in descending order of control effectiveness. The permit applicant should first examine the highest ranked ("top") option. The top ranked options should be established as BACT unless the permit applicant demonstrates to the satisfaction of the permitting authority that technical considerations, or energy, environmental, or economic impacts justify a conclusion that the top ranked technology is not "achievable" in that case. If the most effective control strategy is eliminated in this fashion, then the next most effective alternative should be evaluated, and so on, until an option is selected as BACT.









EPA has broken down this "top down" process into the following five steps:

Step 1: Identify all available control technologies

Step 2: Eliminate technically infeasible options

Step 3: Rank remaining control technologies

Step 4: Evaluate most effective controls and document results

Step 5: Select the BACT

4.1.2 Overview of Control Technology

The use of clean fuels (natural gas and ULSD oil) and combustion controls will minimize air emissions and ensure compliance with applicable emission-limiting standards. Using clean fuels will minimize emissions of SO_2 , sulfuric acid mist (SAM), $PM/PM_{10}/PM_{2.5}$ and other fuel bound contaminants. Combustion controls will minimize the formation of NO_x and the formation of CO and CO by combustor design. Further NO_x reduction will be achieved by water injection during oil firing. The combination of these techniques has been determined to represent BACT on previous projects based on an evaluation of economic, energy, and environmental impacts. The following subsections present a summary of the best available control technology and practices for the Project.

As discussed previously, the GE CTs, and the Siemens CTs were used to evaluate the air emissions and impacts of the Project. The CT vendor has not been selected. However, FPL desires to obtain guarantees of CT performance that will achieve the nominal generation of 200 MW while achieving emissions within the range of the emissions provided for the GE and Siemens CTs. In recent permitting actions, the FDEP has established BACT for heavy-duty simple-cycle industrial gas turbines like the ones proposed for this Project. These decisions established emission rates that were achieved through the use of advanced low-NOx combustors for limiting NO_x, the use of good combustion practices for control of CO and VOCs and clean fuels (natural gas and ULSD oil) for control of SO₂, SAM, PM₁₀ and PM_{2.5}. The BACT proposed for the Project's CTs is consistent with these recent FDEP permits.

The Project CTs will have two modes of operation (dual fuel) for which a BACT analysis has been performed. The results of the analysis have concluded that the following emission limits constitute BACT for the project.

CTs-Natural Gas Fired

- The CTs will utilize state-of-the-art low-NO_X combustion technology which will achieve gas turbine exhaust NO_X levels of no greater than 9 ppmvd corrected to 15 percent O₂
- CO emissions will be limited to 9 ppmvd corrected to 15% O₂ at base load; and good combustion practices will be utilized.



Emission of PM₁₀ and PM_{2.5} will be limited by firing primarily natural gas and 10-percent opacity

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CTs-ULSD Oil Fired

- The CT will utilize water injection to achieve gas turbine exhaust NO_X levels of no greater than 42 ppmvd corrected to 15 percent O₂
- CO emissions will be limited to 20 ppmvd at base load; and good combustion practices will be utilized
- Hours of operation will be limited to an equivalent to 500 hours per year per CT at base load
- Emission of PM₁₀ and PM_{2.5} will be limited by firing ULSD oil and 10 percent opacity

Emergency "Black-Start" Generators

- Emissions meeting the applicable requirement to 40 CFR Subpart IIII, Stationary Compression Ignition Internal Combustion Engines
- Hours of operation will be limited to provide electric power to start a CT if no power is available and will operate like an emergency stationary RICE generator (100 hr/yr)
- Emissions of PM₁₀ and PM_{2.5} will be limited by firing ULSD oil

Fire Pump Engine

- Emissions meeting the applicable requirement of 40 CFR Subpart IIII, Stationary Compression Ignition Internal Combustion Engines
- Hours of operation will be limited to supply water in the event of a fire and will operate like an emergency stationary RICE generator (100 hr/yr)
- Emissions of PM₁₀ and PM_{2.5} will be limited by firing ULSD oil

Table 4-1 presents the proposed BACT emission limits for the Project.

4.2 Non-GHG Control Technology Review – BACT Analysis

4.2.1 Combustion Turbines

Nitrogen Oxides

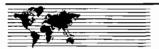
Feasibility

A review of the most recent BACT determinations for similar projects (Appendix Tables D-1 and D-2) demonstrates that emission levels equal to those proposed for the Project, as a result of the proposed low NO_X combustion technology, have been approved by regulatory agencies as BACT for similar simple cycle CTs. Available information suggests that feasible control technologies available, and in order of highest to lowest control efficiency, for simple cycle CTs are as follows:

- 1. Selective catalytic reduction ("Hot" SCR)
- 2. Low NO_X combustion technology
- Wet-injection for oil firing







SCONOxTM was an available technology in the previous decade but has not been installed nor demonstrated on large frame CT such as the "F" class combustion turbines in either simple cycle or more commonly combined cycle configurations. This technology is not considerable available or feasible for simple cycle CTs. Other available technologies such as NOxOut, Thermal DeNOx, NSCR, and XONONTM were evaluated and determined to be technically infeasible or not commercially demonstrated for the Project.

Technology Description

The "Top Down" BACT analysis was performed for the following alternatives:

- 1. Selective catalytic reduction (SCR) and advanced low-NO_x combustors at an emission rate of 2.5 ppmvd corrected to 15 percent O₂ when firing natural gas and 12 ppmvd when firing oil (typical for combined-cycle units).
- 2. Advanced low-NO_x combustors at an emission rate of 9 ppmvd corrected to 15 percent O₂ when firing gas
- 3. Wet Injection at an emission rate of 42 ppmvd corrected to 15 percent O₂ when firing oil

SCR is a post-combustion process where NO_X in the gas stream is reacted with ammonia in the presence of a catalyst to form nitrogen and water. The reaction occurs typically between 600°F and 750°F, which has limited SCR application primarily to combined cycle units where such temperatures occur in the heat-recovery steam generator (HRSG). Exhausts from simple cycle operation range up to 1,200°F, thus limiting the direct application of SCR on this mode of operation. Higher cost ceramic catalyst can accommodate temperatures up to 850 to 1,000°F and application have been installed on aero-derivative gas turbines. Most recently, Mitsubishi Power Systems America (MPSA) installed SCR on four large nominal 200 MW Siemens "F" Class CTs at the Marsh Landing facility in California. This application is natural gas only and required to meet LAER rather than BACT. The MPSA SCR system involves gas cooling to maintain temperatures in range applicable for SCR. In-duct cooling using ambient air would maintain temperatures in the applicable range of SCR with turbine flow of about 2,600,000 acfm and up to 1,200°F temperatures in the exhaust gas. This approach could be accomplished with an electric powered fan rated at about 2,000 hp (1,491 kW) as well as mixing/SCR chamber similar in six to a small HRSG. A similar application when firing distillate oil has not been demonstrated on a "F" Class simple cycle gas turbine.

Ammonium salts (ammonium sulfate and ammonium bisulfate) are formed by the reaction of sulfur oxides in the gas stream and ammonia. These salts are highly acidic, and special precautions in materials and ammonia injection rates must be implemented to minimize their formation. The use of



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natural gas and ULSD limit the potential for ammonium salts to cause corrosion but particulate matter is formed and emitted in the gas stream.

Ammonia injected in the SCR system that does not react with NO_X is emitted directly into the atmosphere and referred to as ammonia slip. In general, SCR manufacturers guarantee ammonia slip to be no more than 10 ppmvd.

While "hot" SCR is technically feasible for the Project, BACT emission levels equivalent to SCR control have not been permitted on similar sized simple cycle CTs by FDEP or any other state agency in EPA Region 4 (see Tables D-1 and D-2).

Low-NO $_{\rm X}$ combustion technology has been offered and installed by manufacturers to reduce NO $_{\rm X}$ emissions by inhibiting thermal NO $_{\rm X}$ formation through premixing fuel and air prior to combustion and providing staged combustion to reduce flame temperatures. NO $_{\rm X}$ emissions of 25 ppmvd (corrected to 15 percent O $_{\rm 2}$) and less have been offered by manufacturers for advanced combustion turbines. Advanced in this context are the larger (over 150 MW) and more efficient (higher initial firing temperatures and lower heat rate) combustion turbines. This technology is truly pollution prevention because NO $_{\rm X}$ emissions are inhibited from forming.

Wet injection was the first combustion technology introduced for combustion turbines (pre-1980s) and was the primary method of reducing NO_X emissions from CTs prior to the 1990s. Indeed, this method of control was first mandated by the NSPS to reduce NO_X levels to 75 ppmvd (corrected to 15 percent O_2 and heat rate). Wet injection is still the primary means of reducing NO_X formation in the combustion process when firing oil. When firing ULSD oil, NO_X is limited by using water injection to 42 ppmvd corrected to 15 percent O_2 .

Although SCONOx™ was commercially available in the late 1990s and early 2000s, it was never demonstrated on "F" Class or larger combustion turbines in either combined cycle or simple cycle modes. The SCONOx™ system has been only operated on a 32 MW facility in California since 1996 and a 5 MW unit in Massachusetts since 1999. The scale up of this complicated technology should not be underestimated. The SCONOx™ technology installed on an "F" Class turbine would involve about a dozen or more different chambers of catalyst for absorption and regeneration. Every 15 to 30 minutes, dampers would be operated to isolate a particular catalyst chamber for regeneration. Each regeneration cycle must isolate the chamber so that O₂ is not introduced and regeneration gas (hydrogen) is introduced. Seal leaks could be significant as applied to the large volume flows associated with a "F" Class turbine. Although the amount of sulfur in natural gas is very low, the SCONOx™ catalyst is poisoned by sulfur compounds, requiring the installation of the SCOSOx™ to







further remove sulfur compounds as part of the overall system. The ability of SCOSOx™ to further remove compounds that will poison the catalyst as part of the overall SCONOx™ system has not been demonstrated when firing ULSD oil. Recent contacts with vendors of SCONOx™ technology have indicated that application of SCONOx has not been applied on large (80 MW or larger) CTs.

The recent permitting trend for advanced simple-cycle combustion turbines is the use of low-NO_X combustors and water injection for ULSD oil firing (see Appendix D, Table D-2). Indeed, the recent simple cycle Florida project, Shady Hills Power Project, L.P. Unit Nos. 4 and 5, have been permitted with this technology in 2012. The Shady Hills project is a GE 7FA.05 CT rated at 210 MW and is allowed to operate 3390 hours per year including 500 hr/yr of ULSD oil.

As discussed previously, the new CTs will be fired with natural gas and ULSD oil will be used not to exceed an equivalent of 500 hr/yr per CT at base load conditions. The following sections present a summary of the economic, environmental, and energy impacts of the available, technically feasible, and demonstrated control technology and emission rate alternatives for the simple cycle units.

Impacts Analysis

Economic—The total capital costs of SCR for the Project exceed \$15,000,000 per CT. The total annualized cost of applying SCR with low-NO $_{\rm X}$ combustion technology ranges from is approximately \$3.3 million to \$2.7 million. The incremental cost effectiveness of adding SCR to the low- NO $_{\rm X}$ combustors and water injection (for oil firing) is estimated at over \$20,000 per ton of NO $_{\rm X}$ removed, based on 3,390 hours of operation with 500 hour of oil firing. Detail calculations (for both GE and Siemens CTs) are provided in Tables 4-2a, 4-2b, 4-3a and 4-3b. It should be noted that CTs associated with the Project are replacements for less efficient GTs with higher NO $_{\rm X}$ emission rates that are operated to supply high demand periods and provide fast-start power for unit outages or other factors that limit base load and intermediate load generation. The typical operation will be less than the potential emissions and therefore the actual cost per ton of NO $_{\rm X}$ removed will be much higher.

Environmental—As discussed in Section 1.0, the Project will replace 36 existing GTs that, with high NO_X emission rates and low stack heights, would not disperse emissions sufficiently to meet the new 1-hour NO₂ NAAQS. The Project will eliminate this potential air quality issue while provide more efficient electric power. The use of low-NO_X combustor technology is truly "pollution prevention". While additional controls beyond low-NO_X combustors (i.e., SCR and SCR with water injection) would further reduce emissions slightly, the effect will not be significant. For example, the installation of hot SCR would reduce potential NO_X emissions by only 150 TPY per CT while causing emissions of







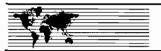
ammonia and ammonium salts, such as ammonium sulfate and bisulfate. Ammonia emissions associated with SCR are expected to be up to 10 ppm based on reported experience; previous permit conditions have specified this level. Indeed, ammonia emissions could be as high as 46.7 TPY per unit at the end of the catalyst's life. Potential emissions of ammonium sulfate and bisulfate will increase emissions of PM_{10} and $PM_{2.5}$; up to 6.4 TPY per unit could be emitted.

The electrical energy required to run the SCR system and the back pressure from the turbine will reduce the available power from the Project. More importantly, the need for tempering air required 2,000 hp (1,491 kW) fans that would require 0.75 percent of the produced power or about 5,054 MWh per year. This power, which would otherwise be available to the electrical system, will have to be replaced. The replacement power will cause air pollutant emissions that would not have occurred without SCR. These "secondary" emissions, coupled with potential emissions of ammonia and ammonium salts, were calculated. As calculated, the net reduction in primary and secondary emissions with SCR when all criteria pollutants are considered will be up to 89 TPY. In addition to criteria pollutants, additional secondary emissions of carbon dioxide would be emitted and were calculated to be 4,746 TPY. As noted, the emissions including CO₂ would be greater with SCR than that proposed using low-NO_X combustion technology.

The replacement of the SCR catalyst will create additional economic and environmental impacts since certain catalysts contain materials that are listed as hazardous chemical wastes under Resource Conservation and Recovery Act (RCRA) regulations (40 CFR 261). In addition, SCR will require the construction and maintenance of storage vessels of anhydrous or aqueous ammonia for use in the reaction. Ammonia has potential health effects, and the construction of ammonia storage facilities triggers the application of at least three major standards: Clean Air Act (Section 112), Occupational Safety and Health Administration (OSHA) 29 CFR 1910.1000, and OSHA 29 CFR 1910.119.

Energy—Significant energy penalties occur with SCR. With SCR, the output of the CT may be reduced by about 1 percent more than with advanced low-NOx combustors. This penalty is the result of the SCR pressure drop, which would be about 10 (according to the SCR template) inches of water and would amount to about 1,560,000 kWh per year in potential lost generation. The energy required by the SCR equipment would be about 6,170,000 kWh per year including the tempering air fan. Taken together, the total lost generation and energy requirements of SCR of 7,740,000 kWh per year could supply the monthly electrical needs of about 645 residential customers. To replace this lost energy, an additional 74,900 British thermal units per year (Btu/yr) or about 75 million cubic feet per year (ft³/yr) of natural gas would be required.





<u>Technology Comparison</u>—The Project will use an advanced heavy-duty industrial gas turbine with advanced low- NO_X combustors. This type of machine advances the state-of-the-art for CTs by being more efficient and less polluting than previous CTs. Integral to the machine's design is low- NO_X combustors that prevent the formation of air pollutants within the combustion process, thereby eliminating the need for add-on controls that can have detrimental effects on the environment. An analogy of this technology is a more efficient automotive engine that gives better mileage and reduces pollutant formation without the need of a catalytic converter.

An advanced gas turbine is unique from an engineering perspective in two ways. First, the advanced machine is larger and has higher initial firing (i.e., combustion) temperatures than conventional turbines. This results in a larger, more thermally efficient machine. For example, the electrical generating capability of the GE Frame 7FA.05 advanced machine is about 221.2 MW compared to the 70 MW to 120 MW conventional machines. The higher initial firing temperature results in about 20 percent more electrical energy produced for the same amount of fossil fuel used in conventional machines. This has the added advantage of producing lower air pollutant emissions (e.g., NO_x, PM, and CO) for each MW generated. While the increased firing temperature increases the thermal NO_x generated, this NO_x increase is controlled through combustor design.

The amount of NO_X control achieved by the low- NO_X combustion technology on an advanced CT is considerably higher than that achieved by a conventional CT. Because of the higher firing initial temperatures, the advanced CT results in greater NO_X emission formation. Since the advanced machine has higher firing temperatures, the NO_X emissions without the use of low- NO_X combustion technology are much higher than a conventional CT (greater than 180 ppmvd vs. 150 ppmvd). This results in an overall greater NO_X reduction on the advanced CT.

The second unique attribute of the advanced machine is the use of low- NO_X combustors that will reduce NO_X emissions to 9 ppmvd when firing natural gas. Thermal NO_X formation is inhibited by using staged combustion techniques where the natural gas and combustion air are premixed prior to ignition. This level of control will result in NO_X emissions of about 0.033 lb/10⁶ Btu when firing gas, which is more than 10 times lower than the existing 36 GTs the Project is replacing.

Since the purpose of the Project is to replace first-generation simple cycle units, it is appropriate to compare the proposed emissions on an equivalent generation basis to that of a conventional CT. The existing gas turbines at the FPL Lauderdale and Port Everglades Plants are first generation aeroderivative turbines using Pratt & Whitney aircraft engines. These units are configured with two gas turbines driving a single gas flow driven turbine coupled to an electric generator and have first generation combustor technology. The heat rates for these GTs are in the range of 17,000 Btu/kWh.



In contrast, the Project will have CTs that have heat rates in the range of 10,000 to 11,000 Btu/kWh at base load conditions. The NO_X emission rates will not only be more than 10 times lower on a heat input basis but more than 15 times lower on a generation basis (i.e., lb NO_X /MWh basis).

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Proposed BACT and Rationale

The proposed BACT for the Project is advanced low-NO_X combustion technology. EPA updated the NSPS for Stationary Combustion Turbines that will commence construction after February 18, 2005. The Subpart KKKK emissions requirements applicable to combustion turbines greater than 30 MW apply to CTs associated with the Project. The NO_X emissions are limited to 15 ppm corrected to 15 percent O_2 or 0.43 lb/MW-hr for natural gas firing and 42 ppm corrected to 15 percent O_2 or 1.3 lb/MW-hr for ULSD oil firing. For the Project, the NO_X emissions are limited to 9 ppm corrected to 15 percent O_2 and about 0.33 lb/MW-hr or less when natural gas firing under base load conditions. NO_X from oil firing will be controlled using water injection (42 ppmvd corrected to 15 percent oxygen). This combination of control technologies is proposed for the following reasons:

- 1. SCR was rejected based on technical, economic, environmental, and energy grounds.
- The estimated incremental cost of SCR is approximately at over \$20,000 per ton of NO_X removed and is similar to cost for other Projects that have rejected SCR as being unreasonable. This is even more apparent if additional pollutant emissions due to SCR are considered.
- 3. Additional environmental impacts would result from SCR operation, including emissions of ammonia; from secondary emissions (to replace the lost generation); and from the generation of hazardous waste (i.e., spent catalyst). While NO_X emissions would be reduced by about 150 TPY per unit with SCR, the net emissions reduction associated with the entire Project would not be as great. There are three additional factors that must be considered:
 - a. The Project replaces 36 less efficient and higher emitting GTs with low stack heights that have concomitantly higher air quality impacts. Emissions are reduced by over a factor of 10 on a heat input basis and by over a factor of 15 on a generation basis.
 - b. SCR will increase direct emissions. Ammonia slip would occur, and it may be as high as 46.7 TPY per unit. Additional particulate matter may be formed through the reaction of ammonia and sulfur oxides forming ammonium salts. As much as 6.4 TPY per unit additional particulate matter may be formed.
 - c. SCR will require energy for system operation and reduce the efficiency of the combustion turbine. This lost energy would have to be replaced because the Project would be an efficient peaking power plant while operating. Any peaking power plants replacing this lost energy would be lower on the dispatch list and inevitably more polluting. Conservatively, this lost energy would result in the emissions of an additional 8.56 TPY of criteria pollutants. Additional emissions of carbon dioxide would also result.







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4. The energy impacts of SCR will reduce potential electrical power generation by more than 5 million kilowatt hours (kWh) per year. This amount of energy is sufficient to provide the monthly electrical needs of 419 residential customers.

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5. The proposed BACT (i.e., low-NO_x combustion technology) provides the most cost effective control alternative, is pollution preventing, and results in low environmental impacts (less than the significant impact levels). Low-NO_x combustion technology at the proposed emissions levels has been adopted previously in BACT determinations. Indeed, compared to existing GTs the Project is replacing, the use of the CTs associated with the Project will result in over 15 times less NO_x emission while producing the same amount of electricity.

Carbon Monoxide and Volatile Organic Compounds

The FDEP has historically established simple cycle CT BACT emission rates based on the use of good combustion practices for minimizing CO and VOC emissions, as add-on CO/VOC controls have been determined to be cost prohibitive. Similarly, CO/VOC add-on controls for the Project have been determined to not be cost effective and BACT is based on good combustion practices.

A review of the most recent BACT determinations for CO for large frame simple-cycle CT projects is provided in Tables D-3 and D-4. Table D-3 demonstrates that FDEP has historically established CT BACT emission rates based on the use of good combustion practices for minimizing CO emissions for simple cycle frame turbines. Although the Department has permitted GE7FA.03 and GE7FA.04 CT models with CO BACT levels as low as 4.1 ppmvd natural gas firing and 8 ppmvd for ULSD oil firing based on operational data, the Project may utilize new GE model 7FA.05 or Siemens F5 turbines for which no operational data exists. The design of the new 7FA.05 differs from the 7FA.03 and 7FA.04 in that power generation has been increased by approximately 20% to over 200 MW at ISO conditions, through higher firing temperature and optimization. The new CT design yields uncertainty that the CO concentrations will be similar to the previous 7FA models. While other BACT determinations have established permit limits as low as 4.1 ppmvd, it has been through supporting operational data of their existing fleet of similar turbines. Because historical operating data are not available for the 7FA.05 and Siemens F5 units, vendor guarantees should be used to establish the BACT limits.



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Feasible Controls

The feasible control technologies, in the order of highest to lowest control efficiency, for simple cycle CTs are as follows:

- Oxidation catalytic reduction (approximately 80% control efficiency)
- Good Combustion Practice including the air-to-fuel ratio and the staging of combustion

Technology Description

Emissions of CO are dependent upon the combustion design, which is a result of the manufacturer's operating specifications, including the air-to-fuel ratio, staging of combustion, and the amount of water injected (i.e., for oil firing). The CTs proposed for the Project have designs to optimize combustion efficiency and minimize CO emissions; however as previously indicated, the GE model 7FA.05 turbines are new CTs with no existing in-service CO test data. Catalytic oxidation is a post-combustion control that has been employed in CO nonattainment areas where regulations have required CO emission levels to be less than those associated with combustion controls alone.

The "Top Down" BACT analysis was performed for the following alternatives:

- Oxidation catalyst at approximately 80 percent removal, resulting in CO concentrations of approximately 2 ppmvd
- Combustion controls at 9 ppmvd when firing natural gas (at base load) and 20 ppmvd when firing oil (at base load)

In an oxidation catalyst control system, CO emissions are reduced by allowing unburned CO to react with oxygen at the surface of a precious metal catalyst, such as platinum. Combustion of CO starts at about 300°F, with an efficiency of 90 percent occurring at temperatures above 600°F. Catalytic oxidation occurs at temperatures 50 percent lower than that of thermal oxidation, which reduces the amount of thermal energy required. For CTs, the oxidation catalyst can be located directly after the CT. Catalyst size depends upon the exhaust flow, temperature, and desired efficiency.

Impact Analysis

Tables 4-5a, 4-5b, 4-6a, and 4-6b present the capital and annualized costs for the GE and Siemens CTs for CO oxidation catalysts. These tables assume total hours per year of operation of 3,390, of which 500 hours is with operation on oil firing. The following summarizes the CO oxidation catalyst cost effectiveness for these scenarios:









- GE 7FA.05 -- CO Oxidation Catalyst Cost Effectiveness 53.3 CO TPY Reduction; \$581,744 per year per CT = \$11,744 per ton CO reduced
- Siemens -- CO Oxidation Catalyst Cost Effectiveness 24.6 CO TPY Reduction; \$589,593 per year per CT = \$28,297 per ton CO reduced

Economic - The capital and annualized cost of a CO oxidation catalyst are approximately \$2,100,000 and \$600,000 per unit, respectively, corresponding to the most cost effective scenario. The resulting cost effectiveness is greater than \$10,000 per ton of CO removed. The cost effectiveness is based on 2,890 hr/yr on natural gas and 500 hours per year of operation on ULSD oil. No costs are associated with combustion techniques since they are inherent in the design. In addition, actual CO emissions are likely to be less than the GE guarantee rates of 9 ppmvd and 20 ppmvd (for gas and oil, respectively) and as a result the cost effectiveness based on actual emissions would be higher than \$11,000 per ton of CO removed. Detail calculations are provided in Tables 4-5a, 4-6a, 4-5b, and 4-6b.

Environmental - The air quality impacts of both oxidation catalyst control and combustion design control techniques are below the significant impact levels for CO. Therefore, no significant environmental benefit would be realized by the installation of a CO catalyst. Moreover, the air quality impacts at the proposed CT emission rate are predicted to be much less than the PSD significant impact levels. The maximum CO impacts are less than 3 percent of the applicable ambient air quality standards. There would also be no secondary benefits, such as reductions in acidic deposition, to reducing CO.

Energy - An energy penalty would result from the pressure drop across the catalyst bed. A pressure drop of about 2 inches water gauge would be expected. At a catalyst back pressure of about 2 inches, an energy penalty of about 1,560,000 kWh/yr would result at 100 percent load, based on the worst case scenario. This energy penalty is sufficient to supply the electrical needs of about 130 residential customers for a year. To replace this lost energy, about 1.6 x 10¹⁰ Btu/yr or about 16 million ft³/yr of natural gas would be required.

Proposed BACT and Rationale

Combustion design is proposed as BACT, as there are adverse technical and economic consequences of using catalytic oxidation on CTs. The proposed BACT emission limits for CO are 9 ppmvd when firing natural gas and 20 ppmvd when firing distillate oil at base load conditions. Catalytic oxidation is considered unreasonable for the following reasons:







- Catalytic oxidation will not produce measurable reduction in the air quality impacts
- The economic impacts are significant (i.e., the capital cost is about \$2.1 million per unit, with an annualized cost of approximately \$600,000 per year per unit)

No existing operational data exists for the new GE 7FA.05 or Siemens F5 turbines necessary to justify CO concentrations less than the vender guarantee. Combustion design is proposed as BACT as a result of the technical and economic consequences of using catalytic oxidation on CTs. Catalytic oxidation is considered unreasonable since it will not produce a measurable reduction in the air quality impacts. The cost of an oxidation catalyst would be significant and not be cost effective given the maximum proposed emission limits, and even less so if actual emissions are less than the value that are guaranteed.

PM/PM₁₀/PM_{2.5}

The PM/PM₁₀/PM_{2.5} emissions from the CTs are a result of incomplete combustion and trace elements in the fuel. The design of the CT ensures that particulate emissions will be minimized by combustion controls and the use of clean fuels. A review of EPA's BACT/LAER Clearinghouse Documents did not reveal any post-combustion particulate control technologies being used on gasfired or oil-fired CTs.

The use of clean fuels, characterized by low PM and trace contaminant contents and advanced combustion techniques, results in negligible PM and PM₁₀ emissions. Emission limits based on the use of clean fuels (i.e., natural gas and ULSD oil) have been established as BACT for PM/PM₁₀ emissions in previous PSD permits.

The maximum particulate emissions from the CT will be lower in concentration than that normally specified for fabric filter designs {i.e., the grain loading associated with the maximum particulate emissions is less than 0.01 grain per standard cubic foot (gr/scf), which is a typical design specification for a baghouse. This further demonstrates that no further particulate controls are necessary for the project.

There are no technically feasible methods for controlling the $PM/PM_{10}/PM_{2.5}$ emissions from CTs, other than the inherent quality of the fuel. Clean fuels, natural gas and distillate oil represent BACT for $PM/PM_{10}/PM_{2.5}$ emissions.





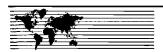


4.2.2 Emergency Black-Start Generators and Fire Pump Engine

The emergency black-start generators and fire pump engine proposed for the Project will utilize clean fuel (i.e., ULSD oil) and good combustion techniques to minimize emissions. The black start emergency generators and fire pump engine will be subject to the requirements of 40 CFR 60 Subpart IIII, Standards of Performance for Stationary Compression Ignition Internal Combustion Engines, published July 11, 2006 and effective on September 11, 2006. For the Project, these units meet the definition of "emergency stationary internal combustion engine" in the NSPS. FPL is proposing to comply with the applicable requirement of 40 CFR Part IIII for these compression ignition engines as BACT for the generators and they would be operated in accordance with Section 60:4211(f).







AMBIENT MONITORING ANALYSIS 5.0

Based on the net emission changes from the proposed Project (see Table 3-3), pre-construction ambient monitoring analyses for PM₁₀, PM_{2.5}, NO₂, CO, and O₃ (based on NO_X or VOC emissions) may be required as part of the PSD application. Ambient monitoring analyses are not required if it can be demonstrated that the Project's maximum air quality impacts will not exceed the PSD significant monitoring concentrations (SMC) and, for O₃, the Project's potential emissions will not exceed 100 TPY of NO_X or VOC emissions.

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Maximum impacts due to the Project only are predicted to be below the SMC for PM₁₀, NO₂ (annual average), and CO (see Tables 6-7 and 6-8). As a result, a pre-construction ambient monitoring analysis is not required for these pollutants as part of the application. It should be noted that EPA has not proposed SMC for the 1-hour average NO₂ concentration.

For O₃, the Project's VOC emissions are less than 100 TPY; however, NO_x emissions are more than 100 TPY or more, which requires that pre-construction ambient monitoring analysis for O₃ be submitted as part of the application.

For PM_{2.5}, on January 22, 2013, the U.S. Court of Appeals vacated the parts of the two PSD rules (40 CFR 51.166 and 40 CFR 52.21) establishing an SMC, finding that EPA was precluded from using the PM_{2.5} SMC to exempt permit applicants from the statutory requirement to compile preconstruction monitoring data. As a result, permitting of new or modified sources requires submittal of monitoring data prior to construction regardless of the source's impact. As a result, PM_{2.5} concentrations from a representative monitor must be submitted as part of the PSD permit application because the Project's PM_{2.5} emissions are greater than the SER.

Based on the impacts of PM₁₀, NO₂, and CO being less than SMC, an exemption from the preconstruction monitoring requirement is applicable pursuant to Rule 62-212.400(3)e, F.A.C. In addition, ambient O₃ and PM_{2.5} monitoring data collected by FDEP at monitoring stations near the Project, are considered to be representative of air quality in the Project's vicinity. These data are being used to satisfy the pre-construction monitoring requirement for O₃ and PM_{2.5} that primarily form from atmospheric processes and are not directly emitted.

Air quality monitoring data collected in Broward County from 2010 through 2012 for O₃ and PM₂₅ are presented in Tables 5-1 and 5-2, respectively. These data indicate that the maximum air quality concentrations measured in the region are well below applicable standards.





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Since the Project's maximum 1-hour average NO₂ and 24-hour PM_{2.5} impacts are predicted to be greater than the significant impact levels for these pollutants (see Tables 6-7 and 6-8, Section 6), more detail analyses are required to demonstrate compliance with the NAAQS for these compounds. For these analyses, total air quality impacts are predicted for the modeled sources which are added to a non-modeled background concentration. The non-modeled background concentrations are estimated from representative ambient air quality monitoring data obtained from air monitoring stations. The 1-hour NO₂ monitoring data collected at monitor ID 012-011-8002 in Dania, Florida, which is the nearest NO₂ monitor to the Lauderdale plant is summarized in Table 5 3.

The $PM_{2.5}$ monitoring presented in Table 5-2 data were collected at monitor ID 012-011-1002 in Davie, Florida, which is the nearest $PM_{2.5}$ monitor to the Lauderdale Plant.



6.0 AIR QUALITY IMPACT ANALYSIS

This section addresses the predicted air quality impacts of regulated air pollutants due to the Project and, as appropriate, background sources. The general modeling approach followed the latest EPA and FDEP modeling guidelines for predicting air quality impacts for regulated pollutants.

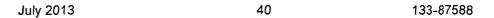
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As described in Section 1.0, the Project replaces 36 GTs located at the Lauderdale and Port Everglades Plants in Broward County. These existing units consist of two aero-derivative gas turbines coupled with a single gas flow driven turbine-electric generator that have low stack heights (less than 50 ft) and high NO_X emissions rates. The low stack heights in proximity to nearby property boundaries result in decreased dispersion properties and, when combined with high NO_X emission rates, result in elevated concentrations of NO₂ concentrations. A 1-hour NAAQS, was recently promulgated by EPA and adopted by FDEP, which is much more stringent than the annual average NAAQS for NO₂. Preliminary modeling analyses of these 36 GT units found that the NO_X emissions from these units would not disperse sufficiently to bring off-site NO₂ concentrations below the 1-hour NO₂ NAAQS. FPL's evaluation concluded that the most cost effective solution is to replace the existing GTs with new, highly efficient combustion turbines with low NO_X emissions. After consultations and agreement with FDEP, FPL plans to bring five new CTs into service by December 31, 2016. The modeling presented in this report provides the impact analysis that would assure 1-hour NO₂ concentrations in the vicinity of the Project do not exceed the NAAQS.

While 24 GTs will be retired at the Lauderdale Plant as a result of the Project, this air quality impact assessment only considered the increase in emissions from the five new CTs and does not address the improvement in the air quality from the retirement of the existing 24 GTs at the Lauderdale Plant or the existing 12 GTs at the Port Everglades Plant. As a result, the analysis results will conservatively reflects the net emissions increase of the overall Project's air quality impact without consideration of the air quality improvements made by retiring the existing GTs. This air quality improvement would occur both in the vicinity of the Project site and at the ENP and result in the expansion of the PSD Increments in the Class II areas in the Project's vicinity and at the ENP PSD Class I area.

Based on the comparison of baseline actual emissions from the existing 24 GTs at the Lauderdale Plant and potential emissions of the Project, the net emissions increases of the Project are greater than the PSD SERs for NO_X , $PM/PM_{10}/PM_{2.5}$, and CO requiring an air quality impact analysis for these pollutants under FDEP rules.







The following sections present a summary of the air quality modeling methodology used for the air quality impact analyses for the proposed Project.

6.1 Air Modeling Analysis Approach and Results – PSD Class II Areas Model Selection

The selection of air quality models to calculate air quality impacts for the proposed project must be based on the models' ability to simulate impacts in the vicinity of the facility. The American Meteorological Society and EPA Regulatory Model (AERMOD) dispersion model was used to evaluate the pollutant impacts due to the proposed project. AERMOD (Version 12345) is available on the EPA's Internet web site, Support Center for Regulatory Air Models (SCRAM), within the Technology Transfer Network (TTN). The EPA and FDEP recommend that AERMOD be used to predict pollutant concentrations at receptors located within 50 km of a source. AERMOD calculates hourly concentrations based on hourly meteorological data. AERMOD is applicable for the type of Project sources and area in which the Project is located since it is recognized as containing the latest scientific algorithms for simulating plume behavior in all types of terrain.

AERMOD was used to predict the maximum pollutant concentrations due to the Project at nearby areas surrounding the facility.

For modeling analyses that will undergo regulatory review, such as determining compliance with NAAQS, the following model features are recommended by EPA for rural mode and are referred to as the regulatory default options in AERMOD:

- 1. Final plume rise at all receptor locations
- 2. Stack tip downwash
- 3. Buoyancy induced dispersion
- 4. Default wind speed profile coefficients for rural mode
- 5. Default vertical potential temperature gradients
- 6. Calm wind processing

The EPA regulatory default options were used to address maximum impacts

Project Sources

Air quality analyses were performed to assess the maximum impacts of the five new simple-cycle CTs at FPL's existing Lauderdale Plant. The CTs being evaluated for the Project are nominal 200 MW units and include the GE 7FA.05 and 7FA.04 CTs, and Siemens F5 CTs (or their equivalents).







The air modeling analyses address air impacts from the GE 7FA.05 and Siemens F5 CTs. Because the GE 7FA.04 CT has lower emissions and slightly lower exit gas temperatures and flow rates over the range of turbine inlet temperatures and loads than those of the GE 7FA.05, the predicted air quality impacts for the GE 7FA.05 CTs are expected to be higher than those for the GE 7FA.04 CT and therefore provide a conservative estimate of the impacts of the GE 7FA.04 CTs.

Summaries of the criteria pollutant emission rates, physical stack and stack operating parameters for the proposed GE 7FA.05 and Siemens F5 CTs used in the air modeling analysis are presented in Section 2 for both natural gas-firing and ULSD oil-firing. For each CT type, impacts were predicted for a range of possible operating conditions. The following 9 CT load and temperature scenarios were evaluated for the GE 7FA.05 CTs when firing natural gas and ULSD oil:

- 100 percent load and ambient temperatures of 35°F, 75°F, and 95°F
- 75 percent load and ambient temperature of 35°F, 75°F, and 95°F
- 50 percent load and ambient temperature of 35°F, 75°F, and 95°F

For Siemens F5 CTs firing natural gas, the following 6 operating scenarios were evaluated in the modeling analysis:

- 100 percent load and ambient temperatures of 35°F, 75°F and 95°F
- 40 percent load and ambient temperature of 35°F and 75°F
- 44 percent load and ambient temperature of 95°F

For Siemens F5 CTs firing ULSD oil, the following 6 operating scenarios were evaluated in the modeling analysis:

- 100 percent load and ambient temperatures of 35°F, 75°F and 95°F
- 50 percent load and ambient temperature of 35°F 75°F and 95°F

The new CTs will have stack heights of 80 feet and an inner diameter of 23 ft. Building downwash effects were included in the modeling analysis to account for the nearby structures. In addition, for cumulative source impact assessments, building downwash effects were included in the modeling analysis for the Lauderdale Plant's existing sources.

The Project also includes four black-start engines (or two existing GTs) which will be used on an emergency basis only to start the new CTs. A fire pump engine will also be installed for emergency purposes. Operation of this equipment is limited to no more than 100 hr/yr for non-emergency situations. These engines are considered intermittant sources based on guidance from the EPA memo "Additional Clarification Regarding Application of Appendix W Modeling Guidance for the





1-Hour NO₂ National Ambient Air Quality Standard (March 1, 2011)." From that guidance, compliance demonstrations should be based on emissions that are continuous or frequent enough to contribute significantly to the annual distribution of daily maximum 1-hour concentrations.

In accordance with this guidance and the recommendations in Section 8.1.1 of Appendix W (40 CFR 51), FDEP was contacted with regards to the operation of the proposed black-start and fire pump engines and agreed that these engines were intermittant sources. Based on the planned intermittant use of the black-start engines, the emissions from these equipment were not modeled in the air impact assessment.

Building Downwash Effects

The dimensions of structures associated with the CTs were provided by the vendors of each type of CT. The primary structures for the CTs are the air inlet structures and the dimensions for each structure are provided in the table below. All structures were processed in the EPA Building Profile Input Program [(BPIP), Version 04274] to determine direction specific structure heights and widths for each 10 degree azimuth direction for each source that was included in the modeling analysis:

Structure	Height (ft)	Width (ft)	Length (ft)
For GE F7A.05 CTs			
CT Air Inlet	72.1	21.4	44.3
CT Building	22	36	30
For Siemens F5 CTs			
CT Air Inlet	75	21.4	44.3
CT Building	22	36	30

Meteorological Data

Meteorological data used in AERMOD to estimate air quality impacts consisted of a concurrent 5-year period of hourly surface weather observations and upper air sounding data collected from the National Weather Service (NWS) stations located at the Fort Lauderdale-Hollywood International Airport (FLL) and Florida International University (FIU) in Miami, respectively. The 5-year period of the meteorological data was from 2006 through 2010 and was prepared by the FDEP using AERMET Version 12345. AERMINUTE Version 11059 was used to process 1-minute wind data collected by the automatic surface observing system (ASOS) into hourly averages of wind direction and wind speed. A minimum wind speed threshold of 0.5 meters per second (m/s) was used. The NWS office at the airport is located approximately 4 km (2.5 miles) due east of the Project site. The areas







between the airport and Lauderdale Plant are flat with very similar land characteristics. As such, the meteorological parameters collected at Fort Lauderdale-Hollywood International Airport are considered to be representative of those that exist at the Project site.

Land use parameters were extracted seasonally and for twelve 30-degree wind direction sectors using AERSURFACE Version 13016. The parameters were taken from the airport (measurement site). The annual average land use parameters for both the airport and application site locations are as follows:

<u>Location</u>	<u>Albedo</u>	Bowen Ratio	Surface Roughness
NWS Station	0.16	0.62	0.075
Project Site	0.17	0.80	0.205

The results indicate that the Project site's land use parameters are similar to those for the NWS station. As such, the meteorological data with land use values from the NWS site were selected to be used throughout the modeling analysis.

Receptor Locations

A Cartesian grid was used to predict concentrations on and beyond the property boundary out to 5 km. Receptors were located at the following intervals and distances from the Project:

- Along the property boundary or fence line 50 meters
- Beyond the fence line to 2 km 100 meters
- From 2 km to 5 km 250 meters

More than 2,000 receptors were used to estimate the maximum concentrations predicted for the Project.

Significant Impact Analysis

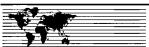
A significant impact analysis is performed to determine the maximum air quality impact due to only the Project's emissions increases. If the highest predicted impact for a particular pollutant and averaging time exceeds the respective PSD Class II significant impact level (SIL), more detailed modeling analyses are required for that pollutant and averaging time to address compliance with the NAAQS and, if applicable, the allowable PSD increment.

For this Project, SIL analyses were performed for the following pollutants and averaging times:

NO₂: 1-hour and annual averages







■ PM₁₀: 24-hour and annual averages

PM_{2.5}: 24-hour and annual averages

CO: 1-hour and 8-hour averages

The SIL analyses for the 1-hour NO_2 , and 24-hour and annual $PM_{2.5}$ concentrations are based on the maximum 5-year average concentrations predicted using 5 years of representative meteorological data. The SIL analyses for the 24-hour PM_{10} and 1-hour and 8-hour CO concentrations are based on the maximum predicted concentrations over the 5-year period. The SIL analyses for the annual average NO_2 and PM_{10} concentrations are based on maximum predicted concentrations for any year over the 5-year period.

The predicted annual average impacts for the significant impact analysis are based on the CTs being limited to 3,390 hr/yr with ULSD oil-firing for each CT limited to 500 hr/yr. For pollutants with higher predicted impacts occurring when firing ULSD oil, the predicted annual impact is based on the maximum of 500 hr/yr of ULSD oil-firing. The short-term impacts are based on an operation of 10 hours per day of ULSD oil firing that conservatively represent operation of the CTs on this fuel. For pollutants with higher predicted impacts occurring when firing natural gas, the predicted annual impact assumes 3,390 hr/yr of natural gas-firing and the short-term impacts assume only natural gas firing.

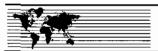
Once the highest impacts were identified for the combination of ambient temperature and operating load condition (i.e., worst-case operating condition), subsequent analyses were performed with the emissions rates and exit gas operating data for those conditions for each pollutant and CT vendor.

It should be noted that In January 2013, the PM_{2.5} SIL under 40 CFR 51.166(k)(2) and 40 CFR 52.21(k)(2) were vacated and remanded the portions of EPA's rule regarding the SIL to exempt sources from cumulative source modeling [Sierra Club v. EPA, 705 F.3d 458 (D.C. Circuit 2013)]. On March 4, 2013, EPA issued *Draft Guidance for PM_{2.5} Permit Modeling* (Stephen D. Page, Director, OAQPS) that provided preliminary recommendations describing how a stationary source seeking a PSD permit can demonstrate that it will not cause or contribute to a violation of the NAAQS and PSD increments. According to the EPA's draft guidance, with additional justification, the permitting authority may use the same PM_{2.5} SILs that were vacated to demonstrate that a full cumulative source impact analysis is not needed.

Based on the results of the significant impact analysis, only the 1-hour NO_2 and 24-hour $PM_{2.5}$ concentrations were predicted to exceed the SIL. When addressing the NAAQS for 1-hour NO_2 , the







5-year averages of the 98th (8th highest) percentile of the daily maximum 1-hour average concentrations at each receptor were determined. The maximum 5-year average of these values is used to estimate the maximum impact. For 24-hour PM_{2.5}, the 5-year average of the 98th (8th highest) percentile of the 24-hour average concentrations at each receptor are determined. The maximum 5-year average of these values is used to estimate the maximum impact.

NO₂ Modeling Analysis

A 3-tiers modeling approach based on the EPA modeling guidance document (Tyler Fox, March 1, 2011; Additional Clarification Regarding Application of Appendix W Modeling Guidance for the 1-hour NO₂ National Ambient Air Quality Standard), a 3-tiered modeling approach is recommended for modeling NO₂ concentrations. These approaches are:

- Tier 1: NO_x emissions are assumed fully converted to NO₂
- Tier 2: NO_X emission are assumed 75 percent converted to NO₂ on an annual basis and 80 percent converted on a 1-hour basis
- Tier 3: an application of a more detailed modeling approach such as Plume Volume Molar Ratio Method (PVMRM) or the Ozone Limited Method (OLM) to further refine NO₂ impacts

For this analysis, a Tier 2 modeling approach was used to predict NO₂ concentrations.

Cumulative Air Quality Analyses

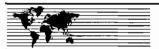
Background concentrations are necessary to determine total ambient air quality impacts to demonstrate compliance with NAAQS. "Background concentrations" are defined as concentrations due to sources other than those specifically included in the modeling analysis. For all pollutants, background would include other point sources not included in the modeling, fugitive emission sources, and natural background sources. In general, monitoring data collected near the area in which the air quality impact is performed is used for this purpose.

Concentrations predicted for the NAAQS analyses include the modeled impacts from sources at the facility, background emission sources including the existing FPL Lauderdale Plant sources, and background concentration that accounts for sources not included in the modeling analysis.

For comparison to the allowable 24-hour PM_{2.5} PSD Class II increment, the highest, second-highest concentration is determined.



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Background NO2 Emission Sources

Current EPA guidance on 1-hour NO₂ NAAQS is provided in the EPA memorandum (Tyler Fox, March 1, 2011, see above). The memorandum suggests that background sources within a radius of 10 km are sufficient for addressing any potential source interactions that could occur during a 1-hour averaging time.

Based on the results of the significant impact analysis, an inventory of background NO₂ emission sources was requested from FDEP. A summary of the emissions, distances and directions of these sources from the proposed project are summarized in Table 6-1. A detailed list of background sources included in the NAAQS modeling analysis is summarized in Table 6-2. The information in Table 6-2 includes the existing Lauderdale Plant sources and FPL Port Everglades Plant.

Background PM_{2.5}Emission Sources

The significant impact area (SIA) for PM_{2.5} was determined to be 4 km, which is the maximum distance to which the Project had a predicted significant impact. This distance was used as the basis for determining the inventory of background sources to be included in the air impact analyses.

EPA and FDEP modeling guidance require that the background source inventory include sources located within and 50 km beyond the SIA. Facilities located within the SIA plus 50 km are summarized in Table 6-3. In order to evaluate sources in the screening area that could significantly interact with the Project facilities in the screening area were evaluated using the North Carolina screening technique (also known as the "20D approach"). Based on this technique, facilities whose annual emissions (i.e., TPY) are less than the threshold quantity, Q, are eliminated from the modeling analysis since they are not likely to significantly interact with the Project. Q is equal to 20 × (D – SIA), where D is the distance in km from the facility to the Project site. A summary of detailed source emissions and stack parameters included in the NAQQS and Class II increment analyses is presented in Table 6-4.

Non-Modeled Background Concentrations

Summaries of measured ambient concentrations, for use in determining background concentrations, are presented in Section 5.0. The background concentrations are based on averages of monitor measurements from 2010 to 2012. The background concentrations used for the 1-hour NO_2 and 24-hour $PM_{2.5}$ NAAQS modeling analyses are 85.3 micrograms per cubic meter ($\mu g/m^3$) and 14.6 $\mu g/m^3$, respectively.



Model Results

Significant Impact/CT Load Analysis – GE 7FA CTs

The results of the CT load analysis for one CT firing natural gas is presented in Table 6-5a and Table 6-5b presents the CT load analysis results for one CT firing ULSD oil. The predicted maximum project-only impacts due to five CTs are compared to the significant impact levels in Table 6-7. Table 6-7 presents conservative results for the CTs firing both natural gas only and ULSD oil only for an entire year (8,760 hr/yr) and firing either natural gas or ULSD oil for part of the day or year. Based on the results presented in Table 6-7, the proposed project's maximum impacts are predicted to be less than the SIL except for the 1-hour NO₂ and 24-hour PM_{2.5} concentrations. As such, cumulative modeling analyses are required for these pollutants and averaging times to determine compliance with the NAAQS and allowable PSD increments.

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Significant Impact/CT Load Analysis – Siemens F5 CTs

The results of the CT load analysis for one CT firing natural gas is presented in Table 6-6a and Table 6-6b presents the CT load analysis results for one CT firing ULSD oil. The predicted maximum project-only impacts due to five CTs are compared to the significant impact levels in Table 6-8. Table 6-8 presents conservative results for the CTs firing both natural gas only and ULSD oil only for the entire year (8,760 hr/yr) firing either natural gas or ULSD oil for part of the day or year. Based on the results presented in Table 6-8, the proposed project's maximum impact are less than the SIL except for 1-hour NO₂ and 24-hour PM_{2.5}. As such, cumulative modeling analyses are required for these pollutants and averaging times to determine compliance with the NAAQS and allowable PSD increments.

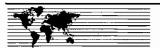
1-hour NO₂ NAAQS Results

The NAAQS modeling results are summarized in Table 6-9. With either Siemens or GE CTs, the maximum predicted 1-hour NO_2 concentration due to all sources is 82.5 μ g/m³, which when added to the background concentration results in a total concentration of 167.8 μ g/m³, which is less than the NAAQS of 188.1 μ g/m³.

24-Hour PM_{2.5} NAAQS Results

The NAAQS modeling results for 24-hour PM_{2.5} are also summarized in Table 6-9. With Siemens CTs, the maximum predicted 24-hour PM_{2.5} concentration due to all sources is $3.2 \,\mu\text{g/m}^3$, which when added to the background concentration of $14.6 \,\mu\text{g/m}^3$ results in a total concentration of $17.8 \,\mu\text{g/m}^3$, which is less than the NAAQS of $35 \,\mu\text{g/m}^3$. With GE CTs, the maximum predicted 24-hour PM_{2.5} concentration due to all sources is $3.1 \,\mu\text{g/m}^3$, which when added to the background concentration of $14.6 \,\mu\text{g/m}^3$ results in a total concentration of $17.7 \,\mu\text{g/m}^3$, which is less than the NAAQS.





24-Hour PM_{2.5} Increment Analysis Results

The PSD increment modeling results for 24-hour PM_{2.5} are summarized in Table 6-10. The maximum predicted 24-hour PM_{2.5} increment is 2.0 and 1.5 μ g/m³, respectively, with Siemens and GE CTs. These concentrations are less than the allowable increment of 9 μ g/m³.

6.2 Air Modeling Analysis Approach and Results- PSD Class I Area Model Selection and General Assumptions

The CALPUFF air modeling system (Version 5.8) was used to predict the Project's maximum air quality concentrations at locations beyond 50 km from the Project. CALPUFF is a non-steady state Lagrangian puff long-range transport model that includes algorithms for chemical transformations (important for visibility controlling pollutants) and wet/dry deposition. CALPUFF was used in a manner that is consistent with methodologies recommended in the following document and in subsequent discussions with the FLM.

■ FLMs' AQRV Workgroup (FLAG) guidance document, revised in October 2010 and referred to as the FLAG Phase I Report

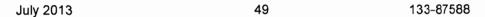
Parameter settings to be used in CALPUFF were based on the latest regulatory guidance. Where the modeling guidance recommends regulatory model defaults, those defaults will be used. For ozone background concentrations, observed hourly ozone data for 2001 to 2003 from CASTNET and AIRS stations will be used. A fixed monthly ammonia background concentration of 0.5 ppb will be used. For predicting 24-hour visibility impairment, the FLAG guidance recommends using CALPOST Version 6.221 Method 8 (MVISBK = 8) and submode 5 (M8_MODE = 5). For this analysis, the background hygroscopic and non-hygroscopic aerosol levels were derived from the 20 percent best natural background days. In addition, parameters will be set to calculate wet and dry (i.e., total) fluxes and concentrations at each evaluated PSD Class I area.

Project Modeled Emissions

The Project's emission, stack, and operating data as well as building dimensions were modeled for the emission sources as indicated previously.

PM emissions for the Project's stack emissions were speciated into filterable and condensable components and into six particle size categories. The effect that each species has on visibility impairment is related to a parameter called the extinction coefficient. The higher the extinction coefficient, the greater is that species' effect on visibility. Filterable PM is speciated into coarse (PMC), fine (PMF), and elemental carbon (EC). The default extinction efficiencies for these species







are 0.6, 1.0, and 10.0, respectively. PMC is PM with aerodynamic diameters greater than 2.5 microns. Both EC and PMF have aerodynamic diameters equal to or less than 2.5 microns. Condensable PM is comprised of sulfate (SO_4) and secondary organic aerosols (SOA). The extinction efficiencies for these species are 3 x f(RH) and 4, respectively, where f(RH) is the relative humidity factor.

The PM group was speciated into filterable and condensable species using the POSTUTIL utility program. Note that emissions for condensable inorganic PM are input directly to CALPUFF as SO₄.

PM speciation (PM_{10} versus $PM_{2.5}$) was developed based on the best available vendor information for the Project's stack sources.

Building Downwash Considerations

The same methods used in the PSD Class II analyses to assess building downwash were used in these analyses.

Meteorological Data

The far-field air modeling analyses were conducted using meteorological and geophysical databases which have been developed for use with the most recent versions of CALPUFF. These datasets were developed using CALMET Version 5.8 and were originally developed by VISTAS and recompiled for Version 5.8 by the FLM. The dataset have 4-km spacing and cover the period from 2001 to 2003. For this Project, meteorological data from VISTAS subdomain No. 2 were used for the far-field modeling analysis.

Receptor Locations

The FLM has developed receptors to represent the boundary and internal areas of all PSD Class I areas. The Class I analysis used the receptors developed by the FLM for ENP.

Significant Impact Analysis

Significant impact analyses were performed to assess the Project's impacts at the PSD Class I area. The maximum predicted NO₂, PM₁₀, and PM_{2.5} concentrations due to the Project were compared to EPA's proposed PSD Class I significant impact levels. If the Project's impacts exceed the proposed EPA PSD Class I significant impact levels, then a more detailed PSD Class I increment analysis will be performed on a pollutant-specific basis. In the PSD Class I incremental analysis, PSD-increment affecting sources will be modeled for comparison to the allowable PSD Class I increments.







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The proposed PSD Class I significant impact levels are:

NO₂: annual average – 0.1 µg/m³

PM₁₀: 24-hour – 0.3 μ g/m³, and annual average – 0.2 μ g/m³

■ $PM_{2.5}$: 24-hour – 0.07 µg/m³, and annual average – 0.06 µg/m³

Model Results

The results of the PSD Class I significant impact analysis for the ENP is presented in Table 6-11. The modeling analysis assumed that the operation of the CTs associated with the Project would operate 24 hours per day for 365 days per year for each fuel. However, the Project is designed to replace existing GTs that operate intermittently depending upon their need to supply peaking and emergency power. Maximum daily operation for the CTs is expected to be no more than 8 to 10 hours per day oil unless there are unique generation requirements. In this case, the maximum impacts are expected to be well below the vacated significant impact levels for the PM_{2.5}. In addition, the new CTs are located in the same location as existing GTs with similar PM_{2.5} emissions as well as over 300 times more SO₂ emissions and over 15 times more NO_X emissions. Both of these air pollutants can become PM_{2.5} through atmospheric reactions. Taking together the predicted air quality impacts and the net reductions of impacts from the existing GTs, the Project will be in compliance with the PM_{2,5} Class I Increments.



7.0 ADDITIONAL IMPACT ANALYSIS

This section presents the impacts that the Project and general commercial, residential, industrial and other growth associated with the Project will have on vegetation, soils, and visibility in the vicinity of the site and impacts at the PSD Class I area of the ENP related to AQRVs. Specifically, this section addresses FDEP Rules 62-212.400(4)(e), (8)(a) and (b), and (9), F.A.C. These rules are:

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- (4) Source Information.
- (e) The air quality impacts, and the nature and extent of any or all general commercial, residential, industrial, and other growth which has occurred since August 7, 1977, in the area the source or modification would affect.
- (8) Additional Impact Analyses.
- (a) The owner or operator shall provide an analysis of the impairment to visibility, soils and vegetation that would occur as a result of the source or modification and general commercial, residential, industrial and other growth associated with the source or modification. The owner or operator need not provide an analysis of the impact on vegetation having no significant commercial or recreational value.
- (b) The owner or operator shall provide an analysis of the air quality impact projected for the area as a result of general commercial, residential, industrial and other growth associated with the source or modification.
- (9) Sources Impacting Federal Class I Areas. Sources impacting Federal Class I areas are subject to the additional requirements provided in 40 CFR 52.21(p), adopted by reference in Rule 62-204.800, F.A.C.

7.1 Potential Impacts Due to Associated Growth

7.1.1 Impacts of Associated Growth

As previously discussed, the Project will replace the 36 existing GTs located at the FPL Lauderdale and Port Everglades Plants. These existing GTs have a capacity of about 1,500 MW and will be replaced with five highly efficient lower emitting CTs with a nominal capacity of 200 MW each, for a total of only 1,000 MW. Thus, the Project is not in response to growth and will provide significant air quality improvement when compared to the existing GTs.

Construction of the proposed Project will occur over approximately 18 to 24 months and will require an average of over 100 workers during that time. It is anticipated that many of these construction personnel will commute to the site. However, no additional permanent workers will be employed for the operation of the facility. The workforce needed to construct and operate the facility represents a small fraction of the population already present in the immediate area. Therefore, while there would be a small increase in vehicular traffic in the area, the effect on air quality levels would be minimal.









There are also expected to be no air quality impacts due to associated commercial and industrial growth. The existing commercial and industrial infrastructure is adequate to provide any support services that facility might require and would not increase with the operation of the facility.

As demonstrated in Section 6.0, the maximum air quality impacts resulting from the proposed new CT Project are predicted to be low and for some pollutants and averaging times, below the significant impact levels for the majority of air pollutant and averaging times. The cumulative 24-hour PM_{2.5} and 1-hour average impacts predicted demonstrate that the Lauderdale Plant and background sources will comply with the PSD increments and NAAQS. In fact, the retirement of 24 GTs at the Lauderdale Plant and another 12 GTs at the Port Everglades Plant is expected to significantly improve air quality in the area.

7.2 Potential Air Quality Effect Levels on Soils, Vegetation, and Wildlife

7.2.1 Soils

The potential and hypothesized effects of atmospheric deposition on soils include:

- Increased soil acidification
- Alteration in cation exchange
- Loss of base cations
- Mobilization of trace metals

The potential sensitivity of specific soils to atmospheric inputs is related to two factors. First, the physical ability of a soil to conduct water vertically through the soil profile is important in influencing the interaction with deposition. Second, the ability of the soil to resist chemical changes, as measured in terms of pH and soil cation exchange capacity (CEC), is important in determining how a soil responds to atmospheric inputs.

7.2.2 Vegetation

The concentrations of the pollutants, duration of exposure, and frequency of exposure influence the response of vegetation to atmospheric pollutants. The pattern of pollutant exposure expected from the facility is that of a few episodes of relatively high ground-level concentration, which occur during certain meteorological conditions, interspersed with long periods of extremely low ground-level concentrations. If there are any effects of stack emissions on plants, they will be from the short-term, higher doses. A dose is the product of the concentration of the pollutant and duration of the exposure.





In general, the effects of air pollutants on vegetation occur primarily from SO₂, NO₂, O₃, and PM. Effects from minor air contaminants, such as fluoride, chlorine, hydrogen chloride, ethylene, ammonia, hydrogen sulfide, CO, and pesticides, have also been reported in the literature. The effects of air pollutants are dependent both on the concentration of the contaminant and the duration of the exposure. The term "injury," as opposed to damage, is commonly used to describe all plant responses to air contaminants and will be used in the context of this analysis. Air contaminants are thought to interact primarily with plant foliage, which is considered to be the major pathway of exposure.

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Injury to vegetation from exposure to various levels of air contaminants can be termed acute, physiological, or chronic. Acute injury occurs as a result of a short-term exposure to a high contaminant concentration and is typically manifested by visible injury symptoms ranging from chlorosis (discoloration) to necrosis (dead areas). Physiological or latent injury occurs as the result of a long-term exposure to contaminant concentrations below those that result in acute injury symptoms. Chronic injury results from repeated exposure to low concentrations over extended periods of time, often without any visible symptoms, but with some effect on the overall growth and productivity of the plant. In this assessment, 100 percent of the particular air pollutant in the ambient air was assumed to interact with the vegetation, which is a very conservative approach.

Nitrogen Dioxide

NO₂ can injure plant tissue with symptoms usually appearing as irregular white to brown collapsed lesions between the leaf veins and near the margins. Conversely, non-injurious levels of NO₂ can be absorbed by plants, enzymatically transformed into ammonia, and incorporated into plant constituents such as amino acids (Matsumaru, et al., 1979).

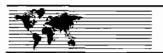
For plants that have been determined to be more sensitive to NO_2 exposure than others, acute exposure (1, 4, and 8 hours) caused 5 percent predicted foliar injury at concentrations ranging from 3,800 to 15,000 $\mu g/m^3$ (Heck and Tingey, 1979). Chronic exposure of selected plants (some considered NO_2 sensitive) to NO_2 concentrations of 2,000 to 4,000 $\mu g/m^3$ for 213 to 1,900 hours caused reductions in yield of up to 37 percent and some chlorosis (Zahn, 1975). Short-term exposure to NO_x at concentrations of 564 $\mu g/m^3$ caused adverse effects in lichen species (Holopainen and Karenlampi, 1984).

Particulate Matter

Although information pertaining to the effects of PM on plants is scarce, baseline concentrations are available (Mandoli and Dubey, 1988). Ten species of native Indian plants were exposed to levels of







PM that ranged from 210 to 366 μ g/m³ for an 8-hour averaging period. Damage in the form of a higher leaf area/dry weight ratio was observed at varying degrees for most plants tested. Concentrations of PM lower than 163 μ g/m³ did not appear to be injurious to the tested plants.

Carbon Monoxide

Information pertaining to the effects of CO on plants is scarce. The main effect of high concentrations of CO is the inhibition of cytochrome c oxidase, the terminal oxidase in the mitochondrial electron transfer chain. Inhibition of cytochrome c oxidase depletes the supply of adenosine triphosphate (ATP), the principal donor of free energy required for cell functions. However, this inhibition only occurs at extremely high concentrations of CO. Pollok, et al. (1989) reported that exposure to a $CO:O_2$ ratio of 25 (equivalent to an ambient CO concentration of $6.85 \times 10^6 \, \mu g/m^3$) resulted in stomatal closure in the leaves of the sunflower (*Helianthus annuus*). Naik, et al. (1992) reported cytochrome c oxidase inhibition in corn, sorghum, millet, and Guinea grass at $CO:O_2$ ratios of 2.5 (equivalent to an ambient CO concentration of $6.85 \times 10^5 \, \mu g/m^3$). These plants were considered the species most sensitive to CO-induced inhibition of cytochrome c oxidase.

Ozone

O₃ can cause various damage to broad-leaved plants including: tissue collapse, interveinal necrosis, and markings on the upper surface leaves know as stippling (pigmented yellow, light tan, red brown, dark brown, red, or purple), flecking (silver or bleached straw white), mottling, chlorosis or bronzing, and bleaching. O₃ can also stunt plant growth and bud formation. On certain plants such as citrus, grape, and tobacco, it is common for leaves to wither and drop early.

7.2.3 Wildlife

A wide range of physiological and ecological effects to fauna has been reported for gaseous and particulate pollutants (Newman, 1981; Newman and Schreiber, 1988). The most severe of these effects have been observed at concentrations above the secondary NAAQS. Physiological and behavioral effects have been observed in experimental animals at or below these standards. For impacts on wildlife, the lowest threshold values of NO_x, and particulates that are reported to cause physiological changes are shown in Table 7-1.

7.2.4 Impact Analysis Methodology

A screening approach was used that compared the Project's maximum predicted ambient concentrations of air pollutants of concern in the vicinity of the site and the ENP PSD Class | Area with effect threshold limits for both vegetation and wildlife as reported in the scientific literature. A literature search was conducted to determine the effects of air contaminants on plant species as



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well as those species reported to occur in the vicinity of the site and in the PSD Class I area. It is recognized that effect threshold information is not available for all species found in these areas, although studies have been performed on a few of the common species and on other species known to be sensitive indicators of effects. Species of lichens, which are symbiotic organisms comprised of green or blue-green algae and fungi, have been used worldwide as air pollution monitors because relatively low levels of sulfur-, nitrogen-, and fluorine-containing pollutants adversely affect many species, altering lichen community composition, growth rates, reproduction, physiology, and morphological appearance (Blett et al., 2003).

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7.3 Impacts on Soils, Vegetation, Wildlife, and Visibility in the Project's Vicinity

7.3.1 Impacts on Vegetation and Soils

Vegetative communities in the vicinity of the plant area are red mangrove (*Rhizophora mangle*), tidal dwarf red mangrove, buttonwood (*Conocarpus erectus*), white mangrove (*Laguncularia racemosa*), and black mangrove (*Avicennia germinans*). The red mangroves that are found in the tidal flats are characteristic of the dwarf mangrove community, reduced in size due to higher salinities and reduced tidal flushing. Additional vegetative species observed within the mangrove community include occasional Brazilian pepper (*Schinus terebinthfolius*), Australian pine (*Casuarina equisetifolia*), tree seaside oxeye (*Borrichia arborescens*), grey nicker (*Caesalpinia bonduc*), groundsel tree (*Baccharis halimifolia*), and cordgrass (*Spartina* sp.).

Soils in the area are primarily histosols, which are peat soils with high amounts of organic matter. The agricultural lands to the west of the site are part of the Everglades Agricultural Area, which is noted for its "muck" (i.e., rich, black soil that is very fertile).

According to the modeling results presented in Section 6.0, the maximum air quality impacts due to the proposed Project are predicted to be below the NAAQS and PSD increments. The NAAQS were established to protect both public health and welfare. Public welfare is protected by the secondary NAAQS, which Florida has adopted. Secondary standards set limits to protect public welfare, including protection against visibility impairment, damage to animals, crops, vegetation, and buildings (EPA, 2007).

Since the project's impacts on the local air quality are predicted to be less than the NAAQS and less than the effect levels on soils and vegetation, the project's impacts on soils, vegetation, and wildlife in the vicinity of the site are expected to be negligible. With regard to O₃ concentrations, the Project's



VOC and NO_x emissions (precursors to O_3 formation) represent an insignificant increase in VOC and NO_x emissions for Broward County.

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7.3.2 Impacts on Wildlife

The major air quality risk to wildlife in the United States is from continuous exposure to pollutants above the National AAQS. This occurs in non-attainment areas. Risks to wildlife also may occur for wildlife living in the vicinity of an emission source that experiences frequent upsets or episodic conditions resulting from malfunctioning equipment, unique meteorological conditions, or startup operations (Newman and Schreiber, 1988). Under these conditions, chronic effects (e.g., particulate contamination) and acute effects (e.g., injury to health) have been observed (Newman, 1981).

Although air pollution impacts to wildlife have been reported in the literature, many of the incidents involved acute exposures to pollutants, usually caused by unusual or highly concentrated releases or unique weather conditions. It is highly unlikely that emissions from the FPL Lauderdale Plant will cause adverse effects to wildlife due to the new CT Project's low impacts, which are predicted to be below the NAAQS based on worst-case operation. Coupled with the mobility of wildlife, the potential for exposure of wildlife to the project's impacts is extremely unlikely. In addition, the Project replaces 36 GTs located at the FPL Lauderdale and Port Everglades Plants in Broward County, which is expected to provide a huge improvement in the air quality of the area.

7.4 Impacts to the ENP PSD Class I Area

7.4.1 Identification of AQRVs and Methodology

An AQRV analysis was conducted to assess the potential risk to AQRVs at the ENP due to the emissions from the proposed Project. The ENP is located between 48.2 and 150 km and to the southwest of the Lauderdale Plant and is the only PSD Class I area located within 200 km.

The U.S. Department of the Interior in 1978 defined AQRVs to be:

- All those values possessed by an area except those that are not affected by changes in air quality and include all those assets of an area whose vitality, significance, or integrity is dependent in some way upon the air environment. These values include visibility and those scenic, cultural, biological, and recreational resources of an area that are affected by air quality.
- Important attributes of an area are those values or assets that make an area significant as a national monument, preserve, or primitive area. They are the assets that are to be preserved if the area is to achieve the purposes for which it was set aside (Federal Register, 1978).







The AQRVs include visibility, freshwater and coastal wetlands, dominant plant communities, unique and rare plant communities, soils and associated periphyton, and the wildlife dependent on these communities for habitat. Rare, endemic, threatened, and endangered species of the national park and bioindicators of air pollution (e.g., lichens) are also evaluated.

7.4.2 Impacts to Soils

The soils of the ENP are generally classified as histosols or entisols. Histosols (peat soils) are organic and have extremely high buffering capacities based on their CEC, base saturation, and bulk density. Therefore, they would be relatively insensitive to atmospheric inputs. The entisols are shallow sandy soils overlying limestone, such as the soils found in the pinelands. The direct connection of these soils with subsurface limestone tends to neutralize any acidic inputs. Moreover, the groundwater table is highly buffered due to the interaction with subsurface limestone formations, which results in high alkalinity (as CaCO₃).

The relatively low sensitivity of the soils to acid inputs, coupled with the low ground-level concentrations of air pollutants predicted from the proposed Project emissions, precludes any significant impact on soils at the ENP.

7.4.3 Impacts to Vegetation

Nitrogen Dioxide

The maximum 1-, 3-, and 8-hour average NO_2 concentrations due to the proposed Project are predicted to be 7.18, 6.13, and 4.66 μ g/m³, respectively, at the ENP. These concentrations are approximately 0.12 to 0.19 percent of the levels that could potentially injure 5 percent of vascular plant foliage (i.e., 3,800 to 15,000 μ g/m³; see previous subsections), and 1.3 percent of the concentration that caused adverse effects in lichen species in acute exposure scenarios (564 μ g/m³; see previous subsections). For a chronic exposure, the maximum annual NO_2 concentration due to the Project is predicted to be 0.008 μ g/m³ at the Class I area, which is less than 0.0004 percent of the levels that caused minimal yield loss and chlorosis in plant tissue (i.e., 2,000 μ g/m³; see previous subsections).

Although it has been shown that simultaneous exposure to SO_2 and NO_2 results in synergistic plant injury (Ashenden and Williams, 1980), the magnitude of this response is generally only 3 to 4 times greater than either gas alone, and usually occurs at unnaturally high levels of each gas. Therefore, the project's predicted concentrations at the ENP are still far below the levels that potentially cause plant injury for either acute or chronic exposure.



Particulate Matter

The maximum 8-hour PM_{10} concentration due to the Project is predicted to be 0.95 μ g/m³ at the ENP. This impact is 0.45 percent of the values that affected plant foliage (i.e., 210 μ g/m³, see previous subsections). As a result, no significant effects to vegetative AQRVs within the ENP are expected as a result of the Project's PM emissions.

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Carbon Monoxide

The maximum 1-hour average concentration due to the project is $2.29 \,\mu\text{g/m}^3$ in the Class I area, which is less than 0.00004 percent of the minimum value that caused inhibition in laboratory studies (i.e., $6.85 \times 10^6 \,\mu\text{g/m}^3$, see previous subsections). The amount of damage sustained at this level, if any, for 1 hour would have negligible effects over an entire growing season. The maximum predicted annual concentration of $0.006 \,\mu\text{g/m}^3$ reflects a more realistic, yet conservative, CO impact level for the Class I area. This maximum concentration is predicted to be less than 9×10^{-7} percent of the value that caused cytochrome c oxidase inhibition $(6.85 \times 10^5 \,\mu\text{g/m}^3)$.

VOC and NOx Emissions and Impacts to Ozone

VOC and NO_x emissions are precursors to O_3 formation. Since the proposed Project includes retirement of 24 GTs at Lauderdale and another 12 GTs at Port Everglades, the VOC and NO_x emissions will actually decrease in Broward County.

Summary

In summary, the phytotoxic effects of the new CT project's emissions within the ENP are expected to be minimal. It is important to note that emissions were evaluated with the assumption that 100 percent was available for plant uptake. This is rarely the case in a natural ecosystem.

7.4.4 Impacts to Wildlife

The Project's low emissions are well below the NAAQS, which are protective of soils, vegetation, and wildlife resources. The maximum predicted impacts of the project in the Class I area are up to six orders of magnitude lower than values of potential impacts to wildlife shown in Table 7-1. No significant effects on wildlife AQRVs from NO_x, CO, PM, or VOCs are expected.

7.4.5 Impacts Upon Visibility

Introduction

The CAA Amendments of 1977 provide for implementation of guidelines to prevent visibility impairment in mandatory Class I areas. The guidelines are intended to protect the aesthetic quality of





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these pristine areas from reduction in visual range and atmospheric discoloration due to various pollutants. Sources of air pollution can cause visible plumes if emissions of PM_{10} and NO_x are sufficiently large. A plume will be visible if its constituents scatter or absorb sufficient light so that the plume is brighter or darker than its viewing background (e.g., the sky or a terrain feature, such as a mountain). PSD Class I areas, such as national parks and wilderness areas, are afforded special visibility protection designed to prevent plume visual impacts to observers within a Class I area.

Visibility is an AQRV for the ENP. Visibility can take the form of plume blight for nearby areas or regional haze for long distances (e.g., distances beyond 50 km). Because the closest approach of the ENP from the Ft. Lauderdale Plant is 48.2 km and all but a small percentage of the ENP is located beyond 50 km from the project site, the change in visibility will be analyzed as regional haze and the following methodology was used to address AQRVs.

Methodology

Based on the FLAG document, current regional haze guidelines characterize a change in visibility by the change in the light-extinction coefficient (b_{ext}). The b_{ext} is the attenuation of light per unit distance due to the scattering and absorption by gases and particles in the atmosphere. A change in the extinction coefficient produces a perceived visual change. An index that simply quantifies the percent change in visibility due to the operation of a source is calculated as:

$$\Delta$$
% = (b_{exts} / b_{extb}) × 100

where: b_{exts} = the extinction coefficient calculated for the source

b_{extb} = the background extinction coefficient

The analysis was conducted in accordance with the most recent guidance from the FLM's AQRV Workgroup (FLAG) Phase I Report (June 27, 2008) (FLAG) document. The purpose of the visibility analysis is to calculate the extinction at each receptor for each day (24-hour period) of the year due to the proposed project. The visibility threshold is a change in extinction of 5 percent (or 0.5 deciviews) and the threshold is not exceeded if the 98th-percentile change in light extinction is less than 5 percent or 0.5 deciview for each modeled year.

Processing of visibility impairment for this study was performed with the California Puff (CALPUFF, Version 5.8) model and the CALPUFF post-processing program CALPOST Version 6.221. The CALPUFF postprocessor model CALPOST is used to calculate the combined visibility effects from the different pollutants that are emitted from the Project. For predicting visibility impairment, the







FLAG guidance recommends using Method 8 (MVISBK = 8) and submode 5 (M8_MODE = 5). For this analysis, the background hygroscopic and non-hygroscopic aerosol levels were derived from the 20 percent best natural background days.

Emissions input to CALPUFF include the maximum rates for SO₂, NO₂, PM, and sulfuric acid mist. Results are provided for both natural gas and ULSD oil firing.

Results

The results of the visibility analysis at the ENP are presented in Table 7-2. When firing natural gas, the maximum predicted visibility impairment is 0.18 dv which is well below the FLM's criteria of 0.5 dv. This value is well below the FLM's recommended screening criterion of 5 percent change. For ULSD oil, the predicted impact is 0.37 dv and 0.41 dv, respectively for GE and Siemens CTs, respectively, based on a conservative 10 hours per day for 365 days per year. As a result, the Project is not expected to have an adverse impact on the existing regional haze at the PSD Class I area of the ENP.

7.4.6 Nitrogen Deposition

General Methods

As part of the AQRV analyses, total nitrogen (N) deposition rate was predicted for the project at the ENP. The deposition analysis criterion is based on the annual averaging period. The total deposition is estimated in units of kilograms per hectare per year (kg/ha/yr) of N. The CALPUFF model is used to predict wet and dry deposition fluxes of various oxides of these elements.

For N deposition, the species include:

- Particulate ammonium nitrate (from species NO₃), wet and dry deposition;
- Nitric acid (species HNO₃), wet and dry deposition;
- Nitrogen oxides (NO_x), dry deposition; and
- Ammonium sulfate (species SO₄), wet and dry deposition.

The CALPUFF model produces results in units of micrograms per square meter per second (µg/m²/s), which are then converted to units of kg/ha/yr.

Deposition analysis threshold (DATs) for total nitrogen deposition of 0.01 kg/ha/yr was provided by the FLM (January 2002). A DAT is the additional amount of nitrogen deposition within a Class I area below which estimated impacts from a new or modified source are considered insignificant. The





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maximum deposition predicted for the project is, therefore, compared to this DATs or significant impact levels.

Results

The maximum predicted total annual nitrogen deposition due to the proposed project at the ENP is summarized in Table 7-3. The maximum annual deposition rate predicted for the project is 0.0036 kg/ha/yr which is well below the FLM's criteria of 0.01 kg/ha/yr.



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TABLES





Table 2-1a: Stack, Operating, and Emission Data for Combustion Turbines (CT)—Natural Gas Combustion GE 7FA.05

					Simple	Cycle Ope	eration			
	•	Base L	oad Turbir	ne Inlet	75% L	oad Turbin	e Inlet	50% Lo	oad Turbin	e Inlet
		T	emperatur	е	Т	emperatur	е	To	emperatur	e
Parameter	Units	35° F	75° F	95° F	35° F	75° F	95° F	35° F	75° F	_ 95° F
CT Stack Data										
Height	ft	80	80	80	80	80	80	80	80	80
Diameter	ft	23	23	23	23	23	23	23	23	23
Temperature	٥F	1,098	1,117	1,132	1,109	1,174	1,209	1,202	1,215	1,215
Velocity	ft/sec	114.69	112.57	108.30	93.10	90.63	88.06	78.83	78.24	78.89
Maximum Hourly Emissi SO₂	gr/100 cf lb/hr	2 13.2	2 12.5	2 11.8	2 10.5	2 10.0	2 9.5	2 8.3	2 8.0	2 7.8
PM ₁₀ /PM _{2.5}	lb/hr	10.6	10.6	10.6	10.6	10.6	10.6	10.6	10.6	10.6
NO _x	ppmvd@15%O2	9	9	9	9	9	9	9	9	9
•	lb/hr	72.0	68.1	64.3	57.0	54.1	52.0	45.2	43.2	42.1
CO	ppmvd@15%O2	7.16	7.26	7.20	7.33	7.08	6.92	7.36	7.50	7.65
	lb/hr	35.0	33.4	31.3	28.2	26.0	24.2	23.0	22.0	22.0
VOC (as methane)	ppmvd@15%O2	1.02	1.03	1.00	1.05	1.00	0.96	1.06	1.06	1.07
	lb/hr	3.4	3.3	3.1	2.7	2.5	2.4	2.2	2.1	2.2
Sulfuric Acid Mist	lb/hr	1.2	1.2	1.1	1.0	0.9	0.9	0.8	0.7	0.7

Source: General Electric Company, 2013 (CT Performance Data); Golder, 2013.



Table 2-1b: Stack, Operating, and Emission Data for Combustion Turbines (CT)—Natural Gas Combustion Siemens F5

				Simple (Cycle Operation	on	
		Base Load Turbine Inlet Temperature			40% Load	d Turbine	44% Load Turbine Inlet Temperature
Parameter	Units	35°F	75°F	95°F	35°F	75°F	95°F
CT Stack Data							
Height	ft	80	80	80	80	80	80
Diameter	ft	23	23	23	23	23	23
Temperature	°F	1,107	1,108	1,127	1,118	1,154	1,176
Velocity	ft/sec	115.6	124.0	118.0	75.5	76.1	76.5
Maximum Hourly Emission SO ₂	gr/100 cf	2	2	2	2	2	2
	lb/hr	12.6	12.9	12.0	6.9	6.9	6.9
PM ₁₀ /PM _{2.5}	lb/hr	9	10	9	8	8	8
NO_x	ppmvd@15%O2	9	9	9	9	9	9
	lb/hr	77	79	74	42	42	42
CO	ppmvd@15%O2	4	4	4	9	9	9
	lb/hr	21	21	20	26	26	26
VOC (as methane)	ppmvd@15%O2	1	1	1	1	1	1
	lb/hr	3.0	3.1	2.9	1.6	1.6	1.6
Sulfuric Acid Mist	lb/hr	1.3	1.3	1.2	0.7	0.7	0.7

Source: Siemens, 2013 (CT Performance Data); Golder, 2013.





Table 2-2a: Stack, Operating, and Emission Data for Combustion Turbines (CT)-ULSD Oil Combustion GE 7FA.05

					Simpl	e Cycle Op	eration			
			oad Turbin emperatur		75% Load Turbine Inlet Temperature			50% Load Turbine Inlet Temperature		
Parameter	Units	35° F	75° F	95° F	35° F	75° F	95° F	35° F	75° F	95° F
CT Stack Data										
Height	ft	80	80	80	80	80	80	80	80	80
Diameter	ft	23	23	23	23	23	23	23	23	23
Temperature	°F	1,107	1,106	1,118	1,143	1,177	1,190	1,215	1,215	1,215
Velocity	ft/sec	109.38	114.03	110.64	90.78	91.65	89.67	75.67	76.14	75.00
Maximum Hourly Emission	ons per Unit									
SO ₂	 %S	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%
-	lb/hr	3.62	3.62	3.42	2.89	2.86	2.72	2.25	2.20	2.09
PM/PM ₁₀ /PM _{2.5}	lb/hr	37.1	37.1	37.1	37.1	37.1	37.1	37.1	37.1	37.1
NO _x	ppmvd@15%O2	42	42	42	42	42	42	42	42	42
^	lb/hr	370.3	369.9	349.4	295.1	291.9	277.2	229.5	224.1	213.6
co	ppmvd@15%O2	13.15	13.61	13.75	13.49	13.31	13.49	13.96	14.26	14.63
	lb/hr	71.0	73.0	70.0	58.0	56.3	54.2	46.4	46.3	45.3
VOC (as methane)	ppmvd@15%O2	2.03	2.08	2.09	3.93	3.98	4.02	3.90	3.93	3.96
	lb/hr	7.99	8.34	8.03	9.61	9.63	9.23	7.41	7.30	7.01
Sulfuric Acid Mist	lb/hr	0.36	0.36	0.34	0.29	0.29	0.27	0.22	0.22	0.21
Lead	lb/hr	0.032	0.032	0.030	0.025	0.025	0.024	0.020	0.019	0.018

Source: General Electric Company, 2013 (CT Performance Data); Golder, 2013.





Table 2-2b: Stack, Operating, and Emission Data for Combustion Turbines (CT)-ULSD Oil Combustion Siemens F5

				Simple C	ycle Operatio	<u> </u>		
			Load Turbin Temperature		50% Load Turbine Inlet Temperat			
Parameter	Units	35°F	75°F	95°F	35°F	75°F	95°F	
CT Stack Data								
Height	ft	80	80	80	80	80	80	
Diameter	ft	23	23	23	23	23	23	
Temperature	°F	1,040	1,067	1,086	1,066	1,112	1,134	
Velocity	ft/sec	118.9	121.5	115.9	83.7	83.1	80.7	
Maximum Hourly Emission	ns per Unit							
SO ₂	%S	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%	
_	lb/hr	3.38	3.34	3.14	2.09	2.03	1.93	
PM/PM ₁₀ /PM _{2.5}	lb/hr	53	52	48	37	35	33	
NO _x	ppmvd@15%O2	42	42	42	42	42	42	
•	lb/hr	378	376	353	235	228	217	
CO	ppmvd@15%O2	9	9	9	100	100	100	
	lb/hr	49.0	49.0	46.0	340.0	331.0	315.0	
VOC (as methane)	ppmvd@15%O2	1	1	1	20	20	20	
, ,	lb/hr	3.1	3.1	2.9	39.0	37.9	36.1	
Sulfuric Acid Mist	lb/hr	0.34	0.33	0.31	0.21	0.20	0.19	
Lead	lb/hr	0.031	0.031	0.029	0.019	0.019	0.018	

Source: Siemens, 2013 (CT Performance Data); Golder, 2013.





Table 2-3a: Summary of Maximum Potential Annual Emissions for the Combustion Turbines GE 7FA.05

								<i>l</i> aximum	Emission	ns (tons/y	rear)		
							Operating Scenario			Operation	g Hours		
							SC-NG 100 % Load	3,390	2,890	2,890	2,890	1,890	2,390
							SC-ULSD 100 % Load	0	500	0	0	0	0
							SC-NG 75 % Load	Ö	0	0	0	0	Ö
							SC-ULSD 75 % Load	0	Ö	500	Ö	Õ	Ô
		Mavimun	. Housh, Es	nissions (lb	/he\		SC-NG 50 % Load	0	0	0	0	1.000	1,000
		Fuel for Am	•	•	,		SC-ULSD 50 % Load	0	0	0	500	500	0
	SC-NG 75 °F	SC-ULSD 75 °F	SC-NG 75 °F	SC-ULSD 75 °F	SC-NG 75 °F	SC-ULSD 75 °F	00 000 00 // 000						
Pollutant	100% Load	100% Load	75% Load	75% Load	50% Load	50% Load	TOTAL	3,390	3,390	3,390	3,390	3,390	3,390
One Combustion Turbine													
SO ₂	12.5	3.6	10.0	2.9	8.0	2.2		21.2	19.0	18.8	18.7	16.4	19.0
PM/PM ₁₀ /PM _{2.5}	10.6	37.1	10.6	37.1	10.6	37.1		18.0	24.6	24.6	24.6	24.6	18.0
NO _x	68.1	369.9	54.1	291.9	43.2	224.1		115.4	190.8	171.3	154.4	141.9	102.9
CO	33.4	73.0	26.0	56.3	22.0	46.3		56.6	66.5	62.4	59.9	54.2	50.9
VOC (as methane)	3.3	8.3	2.5	9.6	2.1	7.3		5.6	6.9	7.2	6.6	6.0	5.0
Sulfuric Acid Mist	1.2	0.4	0.9	0.3	0.7	0.2		2.0	1.8	1.8	1.7	1.5	1.8
Lead	0.0	0.032	0.0	0.025	0.0	0.019		0.00	0.01	0.01	0.00	0.00	0.00
Three Combustion Turbines													
SO ₂	62.7	18.1	49.8	14.3	39.8	11.0		. 106	95	94	93	82	95
PM/PM ₁₀ /PM _{2.5}	53.0	185.5	53.0	185.5	53.0	185.5		90	123	123	123	123	90
NO _x	340.3	1849.4	270.5	1459.3	216.1	1120.4		577	954	857	772	710	515
CO	167.1	365.0	130.0	281.5	110.0	231.6		283	333	312	299	271	255
VOC (as methane)	16.5	41.7	12.7	48.2	10.7	36.5		28.0	34.3	35.9	33.0	30.1	25.1
Sulfuric Acid Mist	5.9	1.8	4.7	1.4	3.7	1.1		9.9	8.9	8.8	8.7	7.7	8.9
Lead	0.00	0.16	0.00	0.12	0.00	0.10		0.00	0.04	0.03	0.02	0.02	0.00

Source: General Electric Company, 2013; Golder, 2013.







Table 2-3b: Summary of Maximum Potential Annual Emissions for the Combustion Turbines Siemens F5

						Maximum	Emission	ns (tons/ye	ar)		
					Operating Scenario			Operatir	a Hours		
					SC-NG 100 % Load	3,390	2,890	0	2,890	1,890	2,390
					SC-ULSD 100 % Load	0	500	Ö	0	250	0
					SC-NG 40 % Load	Ö	0	3390	Ö	1000	1000
					SC-ULSD 50 % Load	0	0	0	500	250	0
	Ma	ximum Hourly	Emiceione	(lh/hr)	30-023D 30 % E0ag	U	Ū	U	300	200	U
		or Ambient Te		• •							
	SC-NG 75 °F	SC-ULSD 75 °F	SC-NG 75 °F	SC-ULSD 75 °F	_						
Pollutant	100% Load	100% Load	40% Load	50% Load	TOTAL	3,390	3,390	3,390	3,390	3,390	3,390
One Combustion Turbine											
SO ₂	12.9	3.3	6.9	2.0		21.8	19.4	11.7	19.1	16.3	18.8
PM/PM ₁₀ /PM _{2.5}	10.0	52.0	8.0	35.0		17.0	27.5	13.6	23.2	24.3	16.0
NO _x	79.0	376.0	42.0	228.0		133.9	208.2	71.2	171.2	171.2	115.4
CO	21.0	49.0	26.0	331.0		35.6	42.6	44.1	113.1	80.3	38.1
VOC (as methane)	3.1	3.1	1.6	37.9		5.3	5.3	2.7	14.0	8.9	4.5
Sulfuric Acid Mist	1.29	0.33	0.69	0.20		2.18	1.94	1.17	1.91	1.63	1.88
Lead	0.0	0.031	0.0	0.019		0.000	0.008	0.000	0.005	0.006	0.000
Three Combustion Turbines											
SO ₂	64.4	16.7	34.5	10.2		109	97	58	96	81	94
PM/PM ₁₀ /PM _{2.5}	50.0	260.0	40.0	175.0		84.8	137.3	67.8	116	122	80
NO _x	395.0	1880.0	210.0	1140.0		670	1,041	356	856	856	577
CO	105.0	245.0	130.0	1655.0		178	213	220	565	402	190
VOC (as methane)	15.50	15.50	8.00	189.50		26.27	26.27	13.56	69.77	44.27	22.52
Sulfuric Acid Mist	6.4	1.7	3.4	1.0		10.9	9.7	5.8	9.6	8.1	9.4
Lead	0.00	0.15	0.00	0.09		0.000	0.038	0.000	0.023	0.031	0.000

Source: General Electric Company, 2013



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Table 2-4: Performance and Emission Data for the Black Start and Fire Pump Diesel Engines

Paramet	ter	Units	Black Start	Engines	Fire Pump
Performa	ance				
	r of Units		1	4	1
Rating		kW	3,100	12,400	
Rating		hp	4,157	16,629	300
Fuel			Diesel	Diesel	Diesel
Fuel He	eat content (HHV)	Btu/lb	19,500	19,500	19,500
Fuel de		lb/gal	7.06	7.06	7.06
Heat in	put (HHV)	MMBtu/hr	29.01	116	2.37
Fuel us	•	gal/hr	210.7	843	17.2
Maximu	ım operation/yr	hours	100	400	100
Maximu	um fuel usage	gal/yr	21,070	84,280	1,720
	arameters .				
Height		ft	30.0	30.0	17
Diamete	er	ft	2.0	2.0	8.0
Temper	rature	°F	893.0	893.0	744
Flow		acfm	24,283	24,283	1,750
<u>Emission</u>	n <u>s</u>				
SO₂-	Basis	%S	0.0015%		0.0015%
	Conversion of S to SO ₂	%	100		100
	Molecular weight SO ₂ / S (64/32)		2		2
	Emission rate	lb/hr	0.045	0.179	0.004
		TPY	0.0022	0.0089	0.0002
NO _x -	Basis	g/hp-hr	5.2		6.8
	Emission rate	lb/hr	47.6	190.3	4.50
		TPY	2.4	9.5	0.22
CO -	Basis	g/hp-hr	0.7		2.6
	Emission rate	lb/hr	6.0	24	1.72
		TPY	0.3	1.2	0.09
VOC -	Basis	g/hp-hr	0.1		1.0
	Emission rate	lb/hr	0.9	4	0.66
		TPY	0.0	0.18	0.03
PM/PM ₁₀	/PM _{2.5} - Basis	g/hp-hr	0.03		0.4
	Emission rate	lb/hr	0.3	1	0.26
		TPY	0.01	0.05	0.01

Source: FPL, 2013; Golder, 2013.

Emissions based on Caterpillar Standby 3,100 kW 60 Hz 900 Diesel Generator (2013) meeting 40 CFR Part 60 Subpart IIII Requirements for Tier 2 engines; 2000 gpm fire pump; 300 ft head, NFPA 20 Certified; Fairbanks Morse Fire Pumps, meeting minimum Subpart IIII NSPS.







Table 2-5a: Summary of Maximum Potential Annual Emissions GE 7FA.05

							Netting Calcula	ations	
		Maximum Potentia	Project al Annual Emiss	ions (TPY)		Maximum 2-Year PSD Average Significant			
	5	4		2 Fuel Oil		from Existing Units b	Change	Emission Rate	PSD Review Required
Pollutant		Black Start Dlesel Engines			TOTAL	(TPY)	(TPY)	(TPY)	rioquirou:
SO ₂	106	0.009	0.000	NA	106	75	32	40	NO
PM	123	0.05	0.01	NA	123	5	118	25	YES
PM ₁₀	123	0.05	0.01	NA	123	5	118	15	YES
PM _{2.5}	123	0.05	0.01	NA	123	5	118	10	YES
NO _x	954	9.51	0.22	NA	964	308	656	40	YES
co	333	1.19	0.09	NA	334	92	242	100	YES
VOC (as methane)	35.9	0.18	0.03	1.10	37.2	1.6	35.6	40	NO
Sulfuric Acid Mist	9.9	Neg.	Neg.	NA	10	11.4	-2	7	NO
Lead	0.040	Neg.	Neg.	NA	0		0.040	0.6	NO
Greenhouse Gases (CO₂e)	445,721	237	19	NA	445,978	76,136	369,842	75,000	YES

^a Based on SC operation for:

Note: Neg.= negligible; NA= not applicable

Source: Golder, 2013.



^{3,390} hours (maximum).

b Based on actual emissions from Annual Operating Reports from 2008-2012.



Table 2-5b: Summary of Maximum Potential Annual Emissions Slemens F5

							Netting Calcu	lations	
		Maximum Potential	Project Annual Emissions	s (TPY)		Maximum 2-Year Average		PSD Significant	PSD
	5	4 Black Start Diesel	Fire Pump	2 Fuel Oil Storage		from Existing Units ^b	Change	Emission Rate	Review Required
Pollutant	CT ª	Engines	Engine	Tanks	TOTAL	(TPY)	(TPY)	(TPY)	
SO ₂	109	0.015	0.000	NA	109	75	34	40	NO
PM	137	0.09	0.01	NA	137	5	133	25	YES
PM ₁₀	137	0.09	0.01	NA	137	5	133	15	YES
PM _{2.5}	137	0.09	0.01	NA	137	5	133	10	YES
NO _x	1.041	16.33	0.22	NA	1.057	308	749	40	YES
CO	565	2.04	0.09	NA	568	92	476	100	YES
VOC (as methane)	69.8	0.31	0.31	1.10	71.5	1.6	69.9	40	YES
Sulfuric Acid Mist	10.9	Neg.	Neg.	NA	11	11.4	-1	7	NO
Lead	0.038	Neg.	Neg.	NA	0		0.038	0.6	NO
Greenhouse Gases (CO₂e)	477,915	1,548	19	NA	479,482	76,136	403,347	75,000	YES

a Based on SC operation for:

3,390 hours (maximum).

Note: Neg.= negligible; NA= not applicable

Source: Golder, 2013.



b Based on actual emissions from Annual Operating Reports from 2008-2012.

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Table 2-6a: Summary of Maximum Potential Annual HAP Emissions **GE 7FA.05**

	N	laximum Potential Annual	Emissions (TPY)		HAP Major Source
Pollutant	5 CTs	4 Black Start Diesel Engines	2 Fuel Oil Storage Tanks	TOTAL	Threshold (TPY)
Total HAPs	7.9	0.009	NA	8.0	25
Single HAP	3.7 ^a	0.005 ^b	NA	3.7	10

Notes: NA= not applicable.

Emissions of total HAPs from fire pump engine are less than 1/2 pound per year.

Source: Golder, 2013

^a Based on formaldehyde emissions ^b Based on benzene emissions

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Table 2-6b: Summary of Maximum Potential Annual HAP Emissions Siemens F5

		Maximum Potential Annual Emissions (TPY)						
Pollutant	5 CTs	3 Black Start Diesel Engines	2 Fuel Oil Storage Tank	Total	Threshold (TPY)			
Total HAPs Single HAP	8.7 4.0 ^a	0.015 0.007 ^a	NA NA	8.7 4.0	25 10			

Notes: NA= not applicable.

Emissions of total HAPs from fire pump engine are less than 1/2 pound per year.

Source: Golder, 2013

^a Based on formaldehyde emissions

^b Based on benzene emissions



Table 3-1: National and Florida AAQS, Allowable PSD increments and Significant Impact Levels

			and Florida 6 (µg/m³)	PS Increment	_		nt Impact (µg/m³)
Pollutant	Averaging Time	Primary Standard	Secondary Standard	Class i	Class II	Class I	Class II
Particulate Matter	Annual Arithmetic Mean	NA	NA NA	4	17	0.2	1
(PM ₁₀) ^a	24-Hour Maximum	150	150	4	30	0.3	5
Particulate Matter	Annual Arithmetic Mean	12	15	1	4	0.06	0.3
(PM _{2.5}) ^a	24-Hour Maximum	35	35	2	9	0.07	1.2
Sulfur Dioxide ^b	Annual Arithmetic Mean	80	NA	2	20	0.1	1
	24-Hour Maximum	365	NA	5	91	0.2	5
	3-Hour Maximum	NA	1,300	25	512	1	25
	1-Hour Maximum	197	NA	NA	NA	NA	7.9 ^e
Carbon Monoxide	8-Hour Maximum	10,000	10,000	NA	NA	NA	500
	1-Hour Maximum	40,000	40,000	NA	NA	NA	2,000
Nitrogen Dioxide ^c	Annual Arithmetic Mean	100	100	2.5	25	0.1	1
	1-Hour Maximum	188	NA	NA	NA	NA	7.6 °
Ozone ^d	1-Hour Maximum	NA	NA	NA	NA	NA	NA
	8-Hour Maximum	147	147	NA	NA	NA	NA
Lead	Rolling 3-Month Average	0.15	0.15	NA	NA	NA	NA

Note: NA = not applicable.

AAQS = ambient air quality standard.

Sources: FR, Vol. 43, No. 118, June 19, 1978; 40 CFR 50; 40 CFR 52.21; Florida Chapter 62.204, F.A.C. Golder, 2013.



a On October 17, 2006, EPA promulgated revised PM₁₀ and PM_{2.5} AAQS; the PM_{2.5} AAQS had been promulgated on July 18, 1997. For PM₁₀, the annual standard was revoked and the 24-hour standard was retain. The 24-hour PM_{2.5} standard was revised to 35 μg/m³ based on the 3-year averages of the 98th percentile values. The annual PM_{2.5} standard of 15 μg/m³, 3-year averages at community monitors, was retained.

b On June 23, 2010, EPA promulgated the 1-hour SQ₂ standard at a level of 75 parts per billion (ppb), based on the 3-year average of the annual 99th percentile of 1-hour daily maximum concentrations (effective August 23, 2010). EPA is also revoking both the existing 24-hour and annual primary SQ₂ standards, effective one year after the designation of an area, pursuant to section 107 of the Clean Air Act.

CON February 9, 2010, EPA promulgated the 1-hour NO2 standard at a level of 100 ppb, based on the 3-year average of the annual 99th percentile of 1-hour daily maximum concentrations (effective April 12, 2010)

d On March 27, 2008, EPA promulgated revised AAQS for ozone. The O₃ standard was modified to be 0.075 ppm (147 μg/m³) for the 8-hour average; achieved when the 3-year average of 99th percentile values is 0.075 ppm or less.

e For NO₂ and SO₂ 1-hour averaging period, an interim Class II significant impact level is shown.

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Table 3-2: PSD Significant Emission Rates and De Minimis Monitoring Concentrations

Pollutant	Regulated Under	Significant Emission Rate (TPY)	De Minimis Monitoring Concentration (µg/m³) ^a
Sulfur Dioxide	NAAQS, NSPS	40	13, 24-hour
Particulate Matter [PM(TSP)]	NSPS	25	NA
Particulate Matter (PM ₁₀)	NAAQS	15	10, 24-hour
Particulate Matter (PM _{2.5}) ^c	NAAQS	10, or	4, 24-Hour
	NAAQS	40 of SO ₂ , or	NA
	NAAQS	40 of NO _X	NA
Nitrogen Dioxide	NAAQS, NSPS	40	14, annual
Carbon Monoxide	NAAQS, NSPS	100	575, 8-hour
Volatile Organic Compounds (Ozone)	NAAQS, NSPS	40 or NO _X	100 TPY⁵
Lead	NAAQS	0.6	0.1, 3-month
Sulfuric Acid Mist	NSPS	7	NM
Total Fluorides	NSPS	3	0.25, 24-hour
Total Reduced Sulfur	NSPS	10	10, 1-hour
Reduced Sulfur Compounds	NSPS	10	10, 1-hour
Hydrogen Sulfide	NSPS	10	0.2, 1-hour
Mercury	NESHAP	0.1	0.25, 24-hour
MWC Organics (dioxin/furans)	NSPS	3.5x10 ⁻⁶	NM
MWC Metals (as PM)	NSPS	15	NM
MWC Acid Gases (SO ₂ + HCI)	NSPS	40	NM
MSW Landfill Gases (as NMOC)	NSPS	50	NM
Greenhouse Gases d		0 (mass basis), and	NM
		75,000 (CO ₂ e basis)	NM

Note: Ambient monitoring requirements for any pollutants may be exempted if the impact of the increase is less than de minimis monitoring concentrations.

NA = not applicable

NM = no ambient measurement method established; therefore, no de minimis

concentration has been established

mg/m³ = micrograms per cubic meter

MWC = municipal waste combustor

MSW = municipal solid waste

NMOC = non-methane organic compounds

Source: 40 CFR 52.21.

Rule 62-212.400, F.A.C.



^a Short-term concentrations are not to be exceeded

^b No *de minimis* concentration; an increase in VOC OR NO_x emissions of 100 TPY or more will require a monitoring analysis for ozone

^c Any emission rate of these pollutants.

^d On July 20, 2011, biogenic CO₂ emissions were deferred from consideration in the significant emission rates for 3 years. This deferral was vacated by the US Court of Appeals on July 12, 2013.

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Table 3-3: Maximum Emission Changes Due to the Project Including Emission Reductions Due to the Existing GT Units 1 Through 24 Compared to the PSD Significant Emission Rates

		Pollutant Emissio	ns
Pollutant	Net Emission Changes* (TPY)	Significant Emission Rate (TPY)	PSD Review
Sulfur Dioxide	34	40	No
Particulate Matter [PM (TSP)]	133	25	Yes
Particulate Matter (PM ₁₀)	133	15	Yes
Particulate Matter (PM _{2.5})	133	15	Yes
Nitrogen Dioxide	749	40	Yes
Carbon Monoxide	476	100	Yes
Volatile Organic Compounds	69.9	40	Yes
Lead	0.04	0.6	No
Sulfuric Acid Mist	-1	7	No
Total Fluorides	NEG	3	No
Total Reduced Sulfur	NEG	10	No
Reduced Sulfur Compounds	NEG	10	No
Hydrogen Sulfide	NEG	10	No
Mercury	NEG	0.1	No
Greenhouse Gases	403,347	75,000	Yes

Note: NEG = Negligible.

* See Table 2-5B.







Pollutant	CT(s)	Fuel	Operating Mode	Proposed BACT Emission Limits	Compliance Methods
NO _x	GE and S ^a GE and S ^a	Natural Gas ULSD Oil	Normal Operation ^b	9 ppmvd at 15% O_2 42 ppmvd at 15% O_2	Initial: EPA Methods- 7E or 20, Continuous Monitoring (Subpart KKKK) Initial: EPA Methods- 7E or 20, Continuous Monitoring (Subpart KKKK)
со	GE and S ^a GE and S ^a	Natural Gas ULSD Oil	Baseload ^b Baseload ^b	9 ppmvd at 15% O ₂ 20 ppmvd	Initial: EPA Method 10 Initial: EPA Method 10
PM/PM ₁₀	GE and S ^a GE and S ^a	Natural Gas ULSD Oil	Normal Operation ^b Normal Operation ^b	10% Opacity 10% Opacity	Initial/Annual: EPA Method 9 Initial/Annual: EPA Method 9
SO ₂ and SAM ^c	GE and S ^a GE and S ^a	Natural Gas ULSD Oil	Normal Operation ^b Normal Operation ^b	-	Initial/Annual: 40 CFR Part 75 Fuel Sampling Initial/Annual: 40 CFR Part 75 Fuel Sampling .

Notes: CT = combustion turbine; ULSD = ultra low sulfur distillate; G = GE 7FA.05 or 7FA.04 CT; S = Siemens F5 CT



^a or equivalent CT.

^b excluding startup, shutdown and fuel switching.

[°] SO₂ and SAM fuel sulfur are proposed to demonstrate non-applicability of PSD and for PM/PM₁₀ PM_{2.5}.

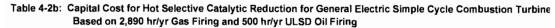


Table 4-2a: Capital Cost for Hot Selective Catalytic Reduction for Siemens Simple Cycle Combustion Turbine Based on 2,890 hr/yr Gas Firing and 500 hr/yr ULSD Oil Firing

Cost Component	Costs	Basis of Cost Component
Direct Capital Costs		
Hot SCR Associated Equipment	10,232,248	Cost of new Entry Estimates for Combustion-Turbine and Combined-Cycle Plants in PJM, 2011
Ammonia Storage Tank	included	
Flue Gas Ductwork	included	
Instrumentation	included	
Emission Monitoring	\$511,612	5% of SCR Associated Equipment
Freight	\$511,612	5% of SCR Associated Equipment
Total Direct Capital Costs (TDCC)	11,255,473	
Direct Installation Costs		
Foundation and supports	\$900,438	8% of TDCC and RCC;OAQPS Cost Control Manual
Handling & Erection	\$1,575,766	14% of TDCC and RCC;OAQPS Cost Control Manual
Electrical	\$450,219	4% of TDCC and RCC;OAQPS Cost Control Manual
Piping (Ammonia Injection Grid)	included	
Insulation for ductwork	\$112,555	1% of TDCC and RCC;OAQPS Cost Control Manual
Painting	\$112,555	1% of TDCC and RCC;OAQPS Cost Control Manual
Site Preparation (General Facilities) Project Contingencies	\$562,774 \$1,125,547	5% of TDCC and RCC;OAQPS Cost Control Manual 10% of TDCC and RCC;OAQPS Cost Control Manual
The section of the se	\$ 1,123,311	
Total Direct Installation Costs (TDIC)	\$4 ,839,853	
Total Capital Costs (TCC)	\$16,095,326	Sum of TDCC and TDIC
Indirect Costs		
Engineering	included	
PSM/RMP Plan	\$50,000	Engineering Estimate
Construction and Field Expense	\$804,766	5% of Total Capital Costs, OAQPS Cost Control Manual
Contractor Fees	\$1,609,533	10% of Total Capital Costs; OAQPS Cost Control Manual
Start-up	\$321,907	2% of Total Capital Costs; OAQPS Cost Control Manual
Performance Tests	\$160,953	1% of Total Capital Costs; OAQPS Cost Control Manual
Total Indirect Capital Cost (TInCC)	\$2,947,159	
Total Direct, Indirect and Capital Costs (TDICC)	\$19,042,485	Sum of TCC and TinCC







Cost Component	Costs	Basis of Cost Component
Direct Capital Costs Hot SCR Associated Equipment Ammonia Storage Tank Flue Gas Ductwork Instrumentation	10,232,248 included included included	Cost of new Entry Estimates for Combustion-Turbine and Combined-Cycle Plants in PJM, 2011
Emission Monitoring Freight	\$511,612 \$511,612	5% of SCR Associated Equipment 5% of SCR Associated Equipment
Total Direct Capital Costs (TDCC)	11,255,473	
Direct Installation Costs Foundation and supports Handling & Erection Electrical Piping (Ammonia Injection Grid) Insulation for ductwork Painting Site Preparation (General Facilities) Project Contingencies Total Direct Installation Costs (TDIC)	\$900,438 \$1,575,766 \$450,219 included \$112,555 \$112,555 \$562,774 \$1,125,547	8% of TDCC and RCC;OAQPS Cost Control Manual 14% of TDCC and RCC;OAQPS Cost Control Manual 4% of TDCC and RCC;OAQPS Cost Control Manual Vendor Estimate 1% of TDCC and RCC;OAQPS Cost Control Manual 1% of TDCC and RCC;OAQPS Cost Control Manual 5% of TDCC and RCC;OAQPS Cost Control Manual 10% of TDCC and RCC;OAQPS Cost Control Manual
Total Capital Costs (TCC)	\$16,095,326	Sum of TDCC and TDiC
Indirect Costs Engineering PSM/RMP Plan Construction and Field Expense Contractor Fees Start-up Performance Tests Total Indirect Capital Cost (TInCC) Total Direct, Indirect and Capital Costs (TDICC)	included \$50,000 \$804,766 \$1,609,533 \$321,907 \$160,953 \$2,947,159	Engineering Estimate 5% of Total Capital Costs; OAQPS Cost Control Manual 10% of Total Capital Costs; OAQPS Cost Control Manual 2% of Total Capital Costs; OAQPS Cost Control Manual 1% of Total Capital Costs; OAQPS Cost Control Manual





Table 4-3a: Annualized Cost for Selective Catalytic Reduction for Siemens Simple Cycle Operation
Based on 2,890 hr/yr Gas Firing and 500 hr/yr ULSD Oil Firing

Cost Component	Costs	Basis of Cost Component
Direct Annual Costs		
Operating Personnel	\$21,840	28 hours/week at \$15/hr
Supervision	\$3,276	15% of Operating Personnel; OAQPS Cost Control Manual
Ammonia	\$33,979	\$556 per ton for anhydrous NH ₃ , 3,390 hr/year
PSM/RMP Update	\$25,000	Engineering Estimate
nventory Cost	\$12,316	Capital Recovery (9.44%) for 1/3 catalyst for SCR
Catalyst Replacement	\$84,125	
Contingency	\$5,416	3% of Direct Annual Costs
Total Direct Annual Costs (TDAC)	\$185,952	
Energy Costs		
Electrical (SCR and Cooling)		330kWh for SCR system and 1,491kWh fan @ \$0.04/kWh, 3,390 hr/yr
MW Loss and Heat Rate Penalty	\$108,963	0.2% of MW output; EPA, 1993 (Page 6-20) ^a and \$3/mmBtu addl fuel costs
Total Energy Costs (TEC)	\$355,891	
Indirect Annual Costs		
Overhead	\$35,457	60% of Operating/Supervision Labor and Ammonia
Property Taxes (exempt)	\$0	0% of Total Capital Costs
nsurance	\$190,425	1% of Total Capital Costs
Administration	\$380,850	2% of Total Capital Costs
Annualized Total Direct Capital	\$2,132,682	10.98% Capital Recovery Factor of 7% over 15 years times sum of TDICC
Total Indirect Annual Costs (TIAC)	\$2,739,414	
Total Annualized Costs Incremental Cost Effectiveness(9 to 3 ppmvd gas	\$3,281,257	Sum of TDAC, TEC and TIAC
and 42 to 14 oil)	\$21,826	NO _x Reduction Only
	\$36,889	Net Emission Reduction

^a Alternative Control Techniques Document--NOx Emissions from Stationary Gas Turbines, Page 6-20.



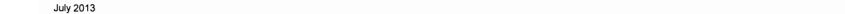


Table 4-3b: Annualized Cost for Selective Catalytic Reduction for General Electric Simple Cycle Operation
Based on 2,890 hr/yr Gas Firing and 500 hr/yr ULSD Oil Firing

Cost Component	Costs	Basis of Cost Component
Direct Annual Costs		
Operating Personnel	\$21,840	28 hours/week at \$15/hr
Supervision	\$3,276	15% of Operating Personnel; OAQPS Cost Control Manual
Ammonia	\$31,099	\$556 per ton for anhydrous NH ₃ , 3,390 hr/year
PSM/RMP Update	\$25,000	Engineering Estimate
Inventory Cost	\$12,316	Capital Recovery (9.44%) for 1/3 catalyst for SCR
Catalyst Replacement	\$84,125	4 years catalyst life; Based on Vendor Budget Estimate
Contingency	\$5,330	3% of Direct Annual Costs
Total Direct Annual Costs (TDAC)	\$182,986	
Energy Costs		
Electrical (SCR and Cooling)	\$246,928	330kWh for SCR system and 1,491kWh fan @ \$0.04/kWh, 3,390 hr/yr
MW Loss and Heat Rate Penalty	\$100,717	0.2% of MW output; EPA, 1993 (Page 6-20) ^a and \$3/mmBtu addl fuel costs
Total Energy Costs (TEC)	\$347,645	
Indirect Annual Costs		
Overhead	\$33,729	60% of Operating/Supervision Labor and Ammonia
Property Taxes (exempt)	\$0	0% of Total Capital Costs
Insurance	\$190,425	1% of Total Capital Costs
Administration	\$380,850	2% of Total Capital Costs
Annualized Total Direct Capital	\$2,132,682	10.98% Capital Recovery Factor of 7% over 15 years times sum of TDICC
Total Indirect Annual Costs (TIAC)	\$2,737,686	
Total Annualized Costs Incremental Cost Effectiveness(9 to 3 ppmvd gas	\$3,268,316	Sum of TDAC, TEC and TIAC
and 42 to 14 oil)	\$23,754	NO _x Reduction Only
		Net Emission Reduction

^a Alternative Control Techniques Document--NOx Emissions from Stationary Gas Turbines, Page 6-20.



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Table 4-4. Maximum Potential Incremental Emissions (TPY) with Selective Catalytic Reduction Based on 2,890 hr/yr Gas Firing and 500 hr/yr ULSD Oil Firing

Incremental Emissions (tons/year) of SCR			
Pollutants	Primary	Secondary	Total
Particulate	6.12	0.27	6.39
Sulfur Dioxide		0.10	0.10
Nitrogen Oxides	-150.33	5.00	-145.34
Carbon Monoxide		3.00	3.00
Volatile Organic Compounds		0.20	0.20
Ammonia	46.71		46.71
Total:	-97.51	8.56	-88.95
Carbon Dioxide (additonal from gas firing)		4 ,745.78	4,745.78





Table 4-5a: Direct and Indirect Capital Costs Oxidation Catalyst for GE Simple Cycle 2,890 hr/yr Natural Gas, 500 hr/yr ULSD Oil Fired

Cost Component	Costs	Basis of Cost Component
Direct Capital Costs	· -	
CO Associated Equipment	\$950,051	Based on Vendor Quote and Construction Cost Index
Auxiliary Equipment (ducts, catalyst housing)		Assumed included
Instrumentation	\$95,005	10% of Oxidation Catalyst Associated Equipment
Freight	\$47,503	5% of Oxidation Catalyst Associated Equipment
Total Direct Capital Costs (TDCC)	\$1,092,558	
Direct Installation Costs		
Foundation and supports	\$87,405	8% of TDCC and RCC;OAQPS Cost Control Manual
Handling & Erection	\$152,958	14% of TDCC and RCC;OAQPS Cost Control Manual
Electrical	\$43,702	4% of TDCC and RCC;OAQPS Cost Control Manual
Piping .	\$21,851	2% of TDCC and RCC;OAQPS Cost Control Manual
Insulation for ductwork	\$10,926	1% of TDCC and RCC;OAQPS Cost Control Manual
Painting	\$10,926	1% of TDCC and RCC;OAQPS Cost Control Manual
Site Preparation	\$54,628	5% Engineering Estimate
Total Direct Installation Costs (TDIC)	\$382,395	
Total Capital Costs	\$1,474,954	Sum of TDCC, TDIC and RCC
Indirect Costs		
Engineering	\$147,495	
Construction and Field Expense	\$73,748	5% of Total Capital Costs; OAQPS Cost Control Manual
Contractor Fees	\$147,495	
Start-up	\$29,499	
Performance Tests	\$14,750	1% of Total Capital Costs; OAQPS Cost Control Manual
Total Indirect Capital Cost (TInDC)	\$412,987	
Contingencies	\$221,243	15% of Total Capital Costs
Total Direct, Indirect and Capital Costs (TDICC)	\$2,109,184	Sum of TCC and TInCC





Table 4-5b: Direct and Indirect Capital Costs Oxidation Catalyst for Siemens Simple Cycle 2,890 hr/yr Natural Gas, 500 hr/yr ULSD Oil Fired

Cost Component	Costs	Basis of Cost Component
Direct Capital Costs		
CO Associated Equipment	\$950,051	Based on Vendor Quote and Construction Cost Index
Auxiliary Equipment (ducts, catalyst housing)	4000,001	Assumed included
Instrumentation	\$95,005	10% of Oxidation Catalyst Associated Equipment
Freight	\$47,503	5% of Oxidation Catalyst Associated Equipment
Total Direct Capital Costs (TDCC)	\$1,092,558	
Direct Installation Costs		
Foundation and supports	\$87,405	8% of TDCC and RCC;OAQPS Cost Control Manual
Handling & Erection	\$152,958	14% of TDCC and RCC;OAQPS Cost Control Manual
Electrical	\$43,702	4% of TDCC and RCC; OAQPS Cost Control Manual
Piping	\$21,851	2% of TDCC and RCC; OAQPS Cost Control Manual
Insulation for ductwork	\$10,926	1% of TDCC and RCC;OAQPS Cost Control Manual
Painting	\$10,926	1% of TDCC and RCC;OAQPS Cost Control Manual
Site Preparation	\$54,628	5% Engineering Estimate
Total Direct Installation Costs (TDIC)	\$382,395	
Total Capital Costs	\$1,474,954	Sum of TDCC, TDIC and RCC
Indirect Costs		
Engineering	\$147,495	10% of Total Capital Costs; OAQPS Cost Control Manual
Construction and Field Expense	\$73,748	5% of Total Capital Costs; OAQPS Cost Control Manual
Contractor Fees	\$147,495	10% of Total Capital Costs; OAQPS Cost Control Manual
Start-up	\$29,499	2% of Total Capital Costs; OAQPS Cost Control Manual
Performance Tests	\$14,750	1% of Total Capital Costs; OAQPS Cost Control Manual
Total Indirect Capital Cost (TInDC)	\$412,987	
Contingencies	\$221,243	15% of Total Capital Costs
Total Direct, Indirect and Capital Costs (TDICC)	\$2,109,184	Sum of TCC and TInCC







Cost Component	Cost	Basis of Cost Estimate
Direct Annual Costs		
Operating Personnel	\$16,425	1/2 hr/shift, \$30/hr, 8760 yr
Supervision	\$2,464	15% of Operating Personnel; OAQPS Cost Control Manual
Maintenance (labor and materials)	\$31,638	1.5% of TDICC, OAQPS Seciton 4
Catalyst Replacement	\$60,321	7 year catalyst life, 50% catalyst replaced
nventory Cost	\$37,200	Capital Recovery (10.98%) for 1/3 catalyst
Contingency	\$7,402	5% of Direct Annual Costs
Total Direct Annual Costs (TDAC)	\$155,450	
Energy Costs		
Heat Rate Penalty	\$100,717	0.2% of MW output; EPA, 1993 (Page 6-20) and \$3/mmBtu addl fuel costs
Total Energy Costs (TDEC)	\$100,717	·
indirect Annual Costs		•
Overhead	\$30,316	60% of Operating/Supervision Labor
Property Taxes (exempt)	\$0	0% of Total Capital Costs
Insurance	\$21,092	•
Administration	\$42,184	2% of Total Capital Costs
Annualized Total Direct Capital	\$231,588	10.98% Capital Recovery Factor of 7% over 15 yrs times sum of TDICC
Total Indirect Annual Costs	\$325,180	
Total Annualized Costs		Sum of TDAC, TEC and TIAC
		Net CO Emission Reduciton
Cost Effectiveness	. ,	per ton of CO Removed
	\$11,744	Net Emission Reduction





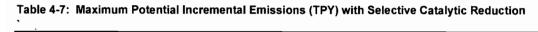


Cost Component	Cost	Basis of Cost Estimate
Direct Annual Costs		
Operating Personnel	\$16,425	, , , -
Supervision	\$2,464	,
Maintenance (labor and materials)	\$31,638	
Inventory Cost	\$37,200	7 year catalyst life, 50% catalyst replaced
Catalyst Replacement		Capital Recovery (10.98%) for 1/3 catalyst
Contingency	\$7,402	5% of Direct Annual Costs
Total Direct Annual Costs (TDAC	\$155,450	
Energy Costs		
Heat Rate Penalty	\$108,963	0.2% of MW output; EPA, 1993 (Page 6-20) and \$3/mmBtu addl fuel costs
Total Energy Costs (TDEC	\$108,963	
Indirect Annual Costs		
Overhead	\$30,316	60% of Operating/Supervision Labor
Property Taxes (exempt)	\$0	0% of Total Capital Costs
Insurance	\$21,092	1% of Total Capital Costs
Administration	\$42,184	
Annualized Total Direct Capital	\$231,588	10.98% Capital Recovery Factor of 7% over 15 yrs times sum of TDICC
Total Indirect Annual Cost	ts \$325,180	
Total Annualized Cost	ts \$589,593	Sum of TDAC, TEC and TIAC
	24.61	Net CO Emission Reduciton
Cost Effectivenes	s \$23,955	per ton of CO Removed
	\$28 297	Net Emission Reduction









•		ssions (TPY) of SCR		
Pollutants		Primary	Secondary	Total
Particulate		2.12	0.05	2.17
Sulfur Dioxide			0.02	0.02
Nitrogen Oxides			0.99	0.99
Carbon Monoxide		-53.32	0.59	-52.72
Volatile Organic Compounds			0.04	0.04
Ammonia		0.00		0.00
	Total:	-51.20	1.69	-49.50
Carbon Dioxide (additional from gas firing)			939.10	939.10





Table 5-1: Summary of Maximum Measured O₃ Concentrations in Vicinity of the FPL Lauderdale Plant, 2010 to 2012

				Conce	entration (µ	g/m³)		
				1-Hour				
		Measuren	nent Period		2nd	4th		
Site No.	Location	Year	Months	Highest	Highest	Highest ^a		
Ozone AAQS	 	-		NA	NA	157		
012-011-8002	7000 N. Ocean Drive	2012	Jan-Dec	164.9	133.5	117.8		
	Dania, FL	2011	Jan-Dec	147.2	115.8	111.9		
		2010	Jan-Dec	141.3	131.5	121.7		
		3-Yr Average				117.1		

Note:

NA = not applicable.

AAQS = ambient air quality standard.

Source: FDEP Quicklook Reports, 2010-2012.



^a The 8-hour O₃ standard is met when the 3-year average of the annual 4th highest of the daily concentration is less than 157 µg/m3.



Table 5-2: Summary of Maximum Measured PM_{2.5} Concentrations in Vicinity of the FPL Lauderdale Plant, 2010 to 2012

					Co	ncentration (µg/m³)	
					24-Ho	ur	Annual ^b
		Measureme	ent Period		2nd		
Site No.	Location	Year	Months	Highest	Highest	98th Percentile ^a	Mean
PM _{2.5} AAQS				NA	NA	35	12
012-011-1002	3205 SW 70th Avenue	2012	Jan-Dec	28.4	21.8	16.7	6.8
	Davie, FL	2011	Jan-Dec	38.5	23.7	13.6	6.5
		2010	Jan-Dec	28.1	25.0	13.5	6.8
		3-Yr Average				14.6	6.7

Note: N

NA = not applicable.

AAQS = ambient air quality standard.

Source: FDEP Quicklook Reports, 2010-2012.



^a The 24-hour PM_{2.5} standard is met when the 3-year average of the 98th percentile of the daily values is less than 35 µg/m³.

 $^{^{\}rm b}$ The annual PM_{2.5} standard is met when the 3-year average of the annual mean values is less than 12 $\mu g/m^3$.





Table 5-3: Summary of Maximum Measured NO₂ Concentrations in Vicinity of the FPL Lauderdale Plant, 2010 to 2012

					Co	ncentration (µg/m³)	
		ur	Annual				
		Measureme	ent Period		2nd		
Site No.	Location	Year	Months	Highest	Highest	98th Percentile ^a	Average
Nitrogen Dioxid	e AAQS			NA	NA	189	100
012-011-8002	7000 N. Ocean Drive	2012	Jan-Dec	143.0	97.8	88.4	9.4
	Dania, F L	2011	Jan-Dec	120.4	101.6	75.2	10.5
		2010	Jan-Dec	122.3	101.6	92.2	13.4
		3-Yr Average				85.3	11.1

Note:

NA = not applicable.

AAQS = ambient air quality standard.

Source: FDEP Quicklook Reports, 2010-2012.



 $^{^{}a}$ The 1-hour NO $_{2}$ standard is met when the 3-year average of the 98th percentile of the daily 1-hour maximum values is less than 189 μ g/m 3 .

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Table 6-1: Summary of the NO₂ Facilities Considered for Inclusion in the Air Modeling NAAQS Analyses

				Rel		Fort Laud	ierdale	Potential NO _x	include in Modeling
Facility ID	Facility Description	East	North	X	Υ		Direction	Emissions	Analysis
		(km)	(km)	(km)	(km)	(km)	(deg)	(TPY)	b
lodeling Area	a (0km - 10km) ^a								
0110037	FLORIDA POWER & LIGHT (PFL)-FT. LAUDERDALE POWER PLANT	580.2	0.9	0.0	0.0	0.00	0	4.868	YES
0112119	WHEELABRATOR SOUTH BROWARD, INC-WHEELABRATOR SOUTH BROWARD	579.5	2.883.3	-0.8	-0.9	1.15	221	1,497	YES
0112736	G & K SERVICES-G & K SERVICES	581.4	2.883.6	1.1	-0.6	1.24	120	6	NO
0111026	HUMANE SOCIETY OF BROWARD COUNTY-HUMANE SOCIETY OF BROWARD COUNTY	583.3	2,882.8	3.0	-1.4	3.29	115	1	NO
0112141	FLORIDA SILICA SAND COMPANY INC-FLORIDA SILICA SAND COMPANY INC	584.2	2,881.2	3.9	-3.0	4.92	128	1	NO
0112149	FRED HUNTER'S MEMORIAL SERVICES INC-FRED HUNTER MEMORIAL CREMATORY FACILITY	578.6	2.878.7	-1.7	-5.5	5.80	197	ND	NO
0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST-MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	581.2	2,877.9	0.9	-6.3	6.33	172	ND	NO
0110054	CITGO PETROLEUM CORP-CITGO - PORT EVERGLADES TERMINAL	586.9	2,885.7	6.6	1.5	6.77	77	8	NO
0110048	MARATHON PETROLEUM COMPANY LP-SPANGLER TERMINAL	587.3	2.885.9	7.0	1.7	7.20	76	ND	NO
0112688	SOUTH FLORIDA MATERIALS CORP. DBA VECENE-VECENERGY - PORT EVERGLADES TERMINAL	587.0	2,885.2	6.7	1.0	6.81	82	10	NO
0110051	BP PRODUCTS NORTH AMERICA, INCBP PRODUCTS - PORT EVERGLADES TERMINAL	587.0	2,886.2	6.7	2.0	7.02	73	ND	NO
0110034	HIGH SIERRA TERMINALING, LLC-HIGH SIERRA TERMINALING, LLC	586.2	2,886.5	5.9	2.3	6.28	69	ND	NO
0110036	FLORIDA POWER & LIGHT (PPE)-PORT EVERGLADES POWER PLANT	587.4	2.885.3	7.1	1.1	7.18	81	33,207	YES
0110056	MOTIVA ENTERPRISES LLC-MOTIVA ENTERPRISES - PT. EV. EAST	587.8	2.886.4	7.5	2.2	7.82	74	ND	NO
0110069	TRANSMONTAIGNE TERMINALS, LLC-TRANSMONTAIGNE - NORTH TERMINAL	586.4	2,886.3	6.1	2.1	6.43	71	ND	NO
0110050	MOTIVA ENTERPRISES LLC-MOTIVA ENTERPRISES - SOUTH	586.8	2,884.6	6.5	0.4	6.51	86	10	NO
0110055	MARATHON PETROLEUM COMPANY LP-MARATHON EISENHOWER TERMINAL	587.4	2,886.6	7.1	2.4	7.48	71	ND	NO
0110053	TRANSMONTAIGNE PRODUCT SERVICES INCTRANSMONTAIGNE PORT EVERGLADES (SOUTH)	587.1	2,885.6	6.8	1.4	6.94	78	12	NO
0110034	HIGH SIERRA TERMINALING, LLC-HIGH SIERRA TERMINALING, LLC	587.1	2,886.6	6.8	2.4	7.21	71	ND	NO
eyound Mode	eling Area (10km - 25km) ^a								
0112078	BROWARD PET CEMETERY INC-BROWARD PET CEMETERY	569.9	2,890.4	-10.4	6.2	12.12	301	ND	NO
0112704	PAS TECHNOLOGIES-PAS TECHNOLOGIES	571.9	2,874.1	-8.4	-10.1	13.14	220	ND	NO
0112146	ATLANTIC BURIAL & CASKET CO-ABCO-FT LAUDERDALE	584.4	2,897.8	4.1	13.6	14.22	17	1	NO
0112152	SCI FUNERAL SERVICES OF FLORIDA INC-GOLD COAST CREMATORY	584.5	2,897.8	4.2	13.6	14.25	17	2	NO
0111019	HOLY CROSS HOSPITAL-HOLY CROSS HOSPITAL	587.1	2,896.5	6.8	12.3	14.07	29	ND	NO
0250603	MIAMI-DADE SOLID WASTE MANAGEMENT-MIAMI DADE SOLID WSTE MGMT/NO DADE LF	570.7	2,872.1	-9.6	-12.1	15.43	219	256	NO
0250664	FLOWERS BAKING COMPANY OF MIAMI, LLCFLOWERS BAKING COMPANY OF MIAMI	579.2	2,868.9	-1.1	-15.3	15.37	184	ND	NO
0112183	STIMPSON COMPANY, INCSTIMPSON COMPANY, INC.	585.5	2,899.5	5.2	15.3	16.16	19	ND	NO
0250407	EXTERIA BUILDING PRODUCTS, LLCEXTERIA BUILDING PRODUCTS	577.5	2,867.5	-2.8	-16.7	16.95	190	ND	NO
0250600	MIAMI-DADE WATER AND SEWER DEPARTMENT-NORTH DISTRICT WASTEWATER TREATMNT PLANT	585.3	2,867.1	5.0	-17.1	17.80	164	459	NO
0250624	GENERAL ASPHALT CO., INCGENERAL ASPHALT PLANT WDHMA	569.7	2,868.3	-10.6	-15.9	19.10	214	81	NO
0251334	TAURUS INTERNATIONAL MANUFACTURING, INCTAURUS INTERNATIONAL	572.1	2,867.0	-8.2	-17.2	19.04	206	5	NO
0110003	W R GRACE & CO-W R GRACE & CO	585.7	2,902.8	5.4	18.6	19.39	16	ND	NO
0251339	AIRCRAFT ELECTRIC MOTORS, INCAIRCRAFT ELECTRIC MOTORS, INC.	570.5	2,867.1	-9.8	-17.1	19.68	210	ND	NO
0110038	OLDCASTLE RETAIL, INCBONSAL AMERICAN	586.2	2,904.6	5.9	20.4	21.24	16	22	NO
0112357	BROWARD COUNTY WATER/WASTEWATER SERVICES-BROWARD COUNTY/NORTH REGIONAL WWTF	584.1	2,905.0	3.8	20.8	21.15	10	88	NO
0250637	REPUBLIC METALS CORPORATION-REPUBLIC METALS CORPORATION	573.9	2,863.6	-6.4	-20.6	21.61	197	ND	NO
0250593	CORDIS CORPCORDIS CORP.	570.3	2,864.9	-10.0	-19.3	21.74	207	ND	NO
0112370	BROWARD CO. WASTE & RECYCLING SERVICES-SOUTHWEST REGIONAL LANDFILL	558.0	2,880.1	-22.3	-4.1	22.66	260	7	NO
7775212	WEEKLEY ASPHALT PAVING, INCWEEKLEY ASPHALT PAVING, INC.	557.3	2,880.6	-23.0	-3.6	23.27	261	ND	NO
0112363	MEDIA PRINTING CORPORATION-MEDIA PRINTING CORPORATION	583.9	2,907.1	3.6	22.9	23.16	9	5	NO
0112094	WASTE MANAGEMENT INC. OF FLORIDA-MONARCH HILL	583.2	2,908.0	2.9	23.8	23.98	7	ND	NO
0112410	SOUTH FLORIDA WATER MANAGEMENT DISTRICT-SFWMD PUMP STATION S-9/S-9A	555.9	2,882.2	-24.4	-2.0	24.52	265	161	NO
0112120	WHEELABRATOR NORTH BROWARD, INCWHEELABRATOR NORTH BROWARD	583.9	2,907.8	3.6	23.6	23.86	9	1,399	NO
	0-PAVEX DEERFIELD PLANT	584.3	2,908.0	4.0	23.8	24.15	9	ND	NO

Note: ND = No data, SID = Significant impact distance for the project

The significant impact distance (SID) for the project is estimated to be:

Fort Lauderdale Facility East and North Coordinates (km) are:

580.3 km 2884.2 km

10 km

EPA recommends that sources to be modeled are expected to have a significant impact in the modeling area. Therefor only sources with 2012 actual annual emissions greater than 30 TPY were included.

^e "Modeling Area" is the area in which the project is predicted to have a significant impact (10 km). EPA recommends that all sources within this area be modeled.

^b Background sources with NO₂ emissions >25 TPY and within 10km of the project location were included in the NAAQS Analysis.

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Table 6-2: Summary of NO₂ Sources Included in the NAAQS Modeling Analyses

				UTM I	_ocation			S	tack Par	ameters				NO ₂ Emis	sion Rate	
Facility	Facility Name		Modeling	X	Y	Hei	ght	Diar	neter	Tempo	erature	Velocity	Stack Parameter	1-H	our	Emissions Data
ID	Emission Unit Description	EU ID	ID Name	(m)	(m)	ft	m	ft	m	°F	К	ft/s m/s	Data Source	(lb/hr)	(g/sec)	Source
0110037 F	LORIDA POWER & LIGHT (PFL)-FT. LAUDERDALE POWER PLANT								_							
	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	035	FLCT4A	580167	2883481.1	150.0	45.72	18.0	5.49	330.0	438.7	48.37		422	53.17	
	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN UNIT)	036	FLCT4B	580,168	2,883,508	150.0	45.72	18.0	5.49	330.0	438.7	48.37		422	53.17	0110037-005-AV
	CCCT WITH HRSG (CT 5A) (PHASE II ACID RAIN UNIT)	037	FLCT5A	580,168	2,883,546	150.0	45.72	18.0	5.49	330.0	438.7	48.37		422	53.17	0 10037-003-AV
	CCCT WITH HRSG (CT 5B) (PHASE II ACID RAIN UNIT)	038	FLCT5B	580,168	2,883,546	150.0	45.72	18.0	5.49	330.0	438.7	48.37		422	53.17	
0112119 V	/HEELABRATOR SOUTH BROWARD, INC-WHEELABRATOR SOUTH BROWARD															
	863 TPD MSW Combustor & Auxiliary Burners- Units 1 - 3	001-003	WHEEL	579,653	2,883,575	275.0	83.82	6.2	1.89	300	422.0	19.43	Title V Renewal Application-2010	342	43.09	Title V Renewal Application-2010
0110036 F	LORIDA POWER & LIGHT (PPE)-PORT EVERGLADES POWER PLANT															
	Unit 5A nominal 250 MW CTG and HRSG	020	CT1A	587,489	2,885,479	149.0	45.42	22.0	6.71	195	363.7	17.74		19.40	2.444	
	Unit 5B nominal 250 MW CTG and HRSG	021	CT1B	587,443	2,885,477	149.0	45.42	22.0	6.71	195	363.7	17.74	January 2012 SCA	19.40	2.444	January 2012 SCA
	Unit 5C nominal 250 MW CTG and HRSG	022	CT1C	587.349	2,885,474	149.0	45.42	22.0	6.71	195	363.7	17.74		19.40	2.444	

Notes

All emission rates are based on worst case senario (Firing fuel oil).



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Table 6-3: Summary of the PM_{2.5} Facilities Considered for Inclusion in the Air Modeling Analyses

			UTM Coo	rdinates	Relative	e to Fort	Lauderdale	Facility ^a	Potential PM _{2.5}	Include i Modeling
Facility ID	Facility Description	Site	East	North	X	Υ		Direction	Emissions	
	, , , , , , , , , , , , , , , , , , , ,		(km)	(km)	(km)	(km)	(km)	(deg)	(TPY)	ь
Modeling Area ^a										
0110037 FLORIDA	POWER & LIGHT (PFL)	FT. LAUDERDALE POWER PLANT	580.0	2883.5	-0.3	-0.7	0.00	0	424.8	YES
0112119 WHEELAI	BRATOR SOUTH BROWARD, INC	WHEELABRATOR SOUTH BROWARD	579.6	2883.3	-0.7	-0.9	1.14	220	103.2	YES
0112736 G & K SEI	RVICES	G & K SERVICES	581.4	2883.6	1.1	-0.6	1.24	120	4.0	NO
0112076 DAVIE CO	DNCRETE CORPORATION	DAVIE CONCRETE CORPORATION	578.7	2884.5	-1.6	0.3	1.67	281	0.0	NO
eyond Modeling Area a										
0112197 WATSON	LABORATORIES, INC - FLORIDA	WATSON LABORATORIES, INC FLORIDA	578.2	2883.6	-2.1	-0.6	2.21	253	5.0	NO
0112074 TRANSFL	O TERMINAL SERVICES, INC. (TTSI)	TRANSFLO FORT LAUDERDALE TERMINAL	583.0	2888.7	2.7	4.5	5.25	31	13.5	NO
0110036 FLORIDA	POWER & LIGHT (PPE)	PORT EVERGLADES POWER PLANT	587.4	2,885.3	7.1	1.1	7.18	81	246	YES
0112127 STEEL FA	ABRICATORS L.L.C.	STEEL FABRICATORS L.L.C.	585.4	2896.0	5.1	11.8	12.79	23	8.7	NO
0250603 MIAMI-DA	DE SOLID WASTE MANAGEMENT	MIAMI DADE SOLID WSTE MGMT/NO DADE LF	570.7	2872.1	-9.6	-12.1	15.43	219	4.8	NO
0112187 CONRAD	YELVINGTON DISTRIBUTORS, INC.	CONRAD YELVINGTON DISTRIBUTORS, INC.	584.6	2899.1	4.3	14.9	15.48	16	17.3	NO
0250407 EXTERIA	BUILDING PRODUCTS, LLC.	EXTERIA BUILDING PRODUCTS	577.5	2867.5	-2.8	-16.7	16.95	190	1.3	NO
0250827 GOODRIG	CH CORPORATION	GOODRICH LANDING SYSTEMS SERVICES	574.5	2867.6	-5.8	-16.6	17.58	199	1.2	NO
0250600 MIAMI-DA	DE WATER AND SEWER DEPARTMENT	NORTH DISTRICT WASTEWATER TREATMNT PLANT	585.3	2867.1	5.0	-17.1	17.86	164	5.5	NO
0112730 R P MINE	RALS	R P MINERALS	585.7	2901.2	5.4	17.0	17.84	18	18.2	NO
0251334 TAURUS	INTERNATIONAL MANUFACTURING, INC.	TAURUS INTERNATIONAL	572.1	2867.0	-8.2	-17.2	19.04	206	3.4	NO
	ONSTRUCTION MATERIALS FLORIDA LLC	CEMEX-PEMBROKE PINES READY-MIX	562.2	2876.7	-18.1	-7.5	19.61	247	1.0	NO
0110009 CEMEX C	ONSTRUCTION MATERIALS FLORIDA LLC	CEMEX NORTH POMPANO FACILITY	586.0	2904.7	5.7	20.5	21.22	16	9.2	NO
	C METALS CORPORATION	REPUBLIC METALS CORPORATION	573.9	2863.6	-6.4	-20.6	21.61	197	5.6	NO
	D CO. WASTE & RECYCLING SERVICES	SOUTHWEST REGIONAL LANDFILL	558.0	2880.1	-22.3	-4.1	22.66	260	1.5	NO
0250803 PANELFO		PANELFOLD, INC.	572.9	2861.9	-7.4	-22.3	23.50	198	4.5	NO
	MANAGEMENT INC. OF FLORIDA	MONARCH HILL	583.2	2908.0	2.9	23.8	23.98	7	33.7	NO
	BRATOR NORTH BROWARD, INC.	WHEELABRATOR NORTH BROWARD	583.9	2907.8	3.6	23.6	23,85	9	96.8	NO
	OCK QUARRIES INC	WHITE ROCK QUARRIES-MAIN QUARRY	564.9	2864.8	-15.4	-19.4	24.78	218	37.2	NO
	CONSTRUCTION INDUSTRIES, INC.	RANGER CONSTRUCTION, SOUTH - MIAMI #2.	558.1	2868.9	-22.2	-15.3	26.97	235	9.3	NO
0111024 HANSON		HANSON ROOF TILE - DEERFIELD BEACH	584.9	2909.2	4.6	25.0	25.46	10	1.8	NO
0250378 QUIKRET		QUIKRETE MIAMI	562.0	2863.9	-18.3	-20.3	27.33	222	1.6	NO
	IDRY MANUFACTURING CORP.	U S FOUNDRY MANUFACTURING CORP.	567.3	2859.8	-13.0	-24.4	27.65	208	10.9	NO
	IANAGEMENT INC. OF FLORIDA	MEDLEY LANDFILL	565.0	2860.0	-15.3	-24.2	28.59	212	37.1	NO
0250020 TARMAC	-	TARMAC-PENNSUCO COMPLEX	562.3	2861.7	-18.0	-22.5	28.83	219	73.4	NO
	DE WATER AND SEWER DEPARTMENT	HIALEAH/PRESTON WATER TREATMENT PLANT	571.4	2856.9	-8.9	-27.3	28.72	198	21.5	NO
0250665 H & J ASF		H & J ASPHALT PLANT	575.1	2855.0	-5.2	-29.2	29.66	190	1.1	NO
	ASPHALT CO., INC.	GENERAL ASPHALT (PLANT #1)	568.8	2855.4	-11.5	-28.8	31.01	202	6.6	NO
	DE CO. DEPT. OF SOLID WASTE MGMT	MIAMI-DADE COUNTY RRF/COVANTA	563.8	2857.6	-16.5	-26.6	31.27	212	58.0	NO
	MEMORIAL HOSPITAL	JACKSON MEMORIAL HOSPITAL	578.0	2852.7	-2.3	-20.0	31.54	184	1.3	NO
	MENT OF VETERANS AFFAIRS	VA MEDICAL CENTER	578.6	2852.6	-2.3 -1.7	-31.6	31.65	183	4.4	NO
	ENUE INVESTMENTS, INC.		563.8	2852.1	-1.7 -16.5	-32.1	36.05	207	2.2	NO
	DE WATER AND SEWER DEPARTMENT	H & R PAVING CENTRAL DISTRICT WASTEWATER TRIMNT PLANT	584.5	2847.8	4.2	-32.1 -36.4	36.66	173	2.4	NO
	MATERIALS COMPANY	FLORIDA ROCK INDUSTRIES INC DIVISION	559.1	2853.3	-21.3	-30.4	37.48	215	2.4	NO
	ONSTRUCTION MATERIALS FL. LLC.	MIAMI CEMENT PLANT	559.1 557.5	2852.0	-21.3 -22.8	-30.9	37.40	215 215	314.6	NO
	ES ASPHALT COMPANY					-32.2 39.6	39.43 40.88		314.6 7.9	
		HARDRIVES / DELRAY PLANT	590.6	2923.8 2843.5	10.3		40.88 42.52	15 197	7.9 12.9	NO
	DE WATER AND SEWER DEPARTMENT	ALEXANDER ORR WATER TREATMENT PLANT	568.0		-12.3	-40.7				NO
	LORIDA WATER MANAGEMENT DISTRICT	SFWMD / PUMP STATION G-335	552.6	2922.0	-27.7	37.8	46.85	324	4.5	NO
0990095 BETHESD	DA MEMORIAL HOSPITAL	BETHESDA MEMORIAL HOSPITAL	592.6	2931.9	12.3	47.7	49.29	14	1.7	NO

ND = No data, SID = Significant impact distance for the project

Fort Lauderdale Facility East and North Coordinates (km) are: The significant impact distance for the project is estimated to be: 2884.20 km



^a "Modeling Area" is the area in which the project is predicted to have a significant impact (2 km). EPA recommends that all sources within this area be modeled.

^b Background sources with PM2.5 emissions > 1 TPY and within 2 km of the project location were included in the NAAQS Analysis.

Table 6-4: Summary of PM_{2.5} Sources Included in the NAAQS Modeling Analyses

				UTM L	ocation			S	tack Par	ameters					PM _{2.5} Emis	ssion Rate	
Facility	Facility Name		Modeling	x	Y	Heig	ght	Diar	neter	Temp	erature	Velo	ocity	Stack Parameter	1-H	our	Emissions Data
ID	Emission Unit Description	EU ID	ID Name	(m)	(m)	ft	m	ft	m	°F	K	ft/s	m/s	Data Source	(lb/hr)	(g/sec)	Source
0110037 F	LORIDA POWER & LIGHT (PFL)-FT. LAUDERDALE POWER PLANT											_			_		
	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	035	FLCT4A	580,167	2,883,481	150.0	45.72	18.0	5.49	330.0	438.7	158.7	48.4		58	7.31	
	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN UNIT)	036	FLCT4B	580,168	2,883,508	150.0	45.72	18.0	5.49	330.0	438.7	158.7	48.4	Title V Renewal Application-2008	58	7.31	0110037-005-AV
	CCCT WITH HRSG (CT 5A) (PHASE II ACID RAIN UNIT)	037	FLCT5A	580,168	2,883,546	150.0	45.72	18.0	5.49	330.0	438.7	158.7	48.4	Title V Netlewal Application-2000	58	7.31	0110007 000711
	CCCT WITH HRSG (CT 5B) (PHASE II ACID RAIN UNIT)	038	FLCT5B	580,168	2,883,546	150.0	45.72	18.0	5.49	330.0	438.7	158.7	48.4		58	7.31	
0112119 W	WHEELABRATOR SOUTH BROWARD, INC-WHEELABRATOR SOUTH BROWARD																
	863 TPD MSW Combustor & Auxiliary Burners- Units 1 - 3	001-003	WHEEL	579,653	2,883,575	275.0	83.82	6.2	1.89	300	422.0	63.8	19.4	Title V Renewal Application-2010	103	13.00	0112119-014-AV
0110036 FI	LORIDA POWER & LIGHT (PPE)-PORT EVERGLADES POWER PLANT																
	Unit 5A nominal 250 MW CTG and HRSG	020	CT1A	587,489	2,885,479	149.0	45.42	22.0	6.71	195	363.7		17.74		13.7	1.73	
	Unit 5B nominal 250 MW CTG and HRSG	021	CT1B	587,443	2,885,477	149.0	45.42	22.0	6.71	195	363.7		17.74	January 2012 SCA	13.7	1.73	January 2012 SCA
	Unit 5C nominal 250 MW CTG and HRSG	022	CT1C	587,349	2,885,474	149.0	45.42	22.0	6.71	195	363.7		17.74		13.7	1.73	

Notes:

All emission rates are based on worst case senario (Firing fuel oil).



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Table 6-5a: Maximum Concentrations Predicted for Emissions of One CT Firing Natural Gas in Simple-Cycle Operation, Lauderdale (GE7FA.05 Units)

Natural Gas		Maximum	Emission R	ates for CT (lb/hr) by Oı	perating Loa	d and Air Te	mperature					Maximum Pr	redicted Conc	entrations (μα	ı/m³) for CT b	ov Operating L	oad and Air T	emperature ⁵	a
		Base Load			75% Load			50% Load		Averaging			Base Load		· · · · · ·	75% Load	, , <u>u</u>		50% Load	
	35°F	75°F	95°	35°F	75°F	95°	35°F	75°F	95°	Time		35°F	75°F	95°	35°F	75°F	95°	35°F	75°F	95°
Seneric ^b	79.37	79.37	79.37	79.37	79.37	79.37	79.37	79.37	79.37	Annual ^c	:	0.13	0.13	0.14	0.16	0.16	0.16	0.19	0.19	0.19
10 g/s) - 2 g/	s/CT									Annual ^d	1	0.09	0.09	0.10	0.12	0.12	0.12	0.14	0.14	0.14
										24-Hour ^c	;	1.01	1.02	1.06	1.26	1.28	1.31	1.47	1.48	1.47
										24-Hour d	1	0.77	0.78	0.81	0.98	0.99	1.01	1.15	1.15	1.14
										8-Hour °	:	2.28	2.32	2.41	2.87	2.91	2.97	3.34	3.36	3.33
										3-Hour ^c	;	2.59	2.63	2.72	3.19	3.23	3.29	3.66	3.68	3.65
										1-Hour ^c	:	2.86	2.90	3.02	3.55	3.59	3.66	4.07	4.09	4.06
										1-Hour [₫]	1	2.44	2.48	2.58	3.09	3.13	3.20	3.61	3.63	3.60
missions for		,																		
PM ₁₀	10.60	10.60	10.60	10.60	10.60	10.60	10.60	10.60	10.60	Annual ^c	•	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.02
										24-Hour ^c	:	0.13	0.14	0.14	0.17	0.17	0.17	0.196	0.197	0.19
PM _{2.5}	10.60	10.60	10.60	10.60	10.60	10.60	10.60	10.60	10.60	Annual ^d	ı	0.01	0.01	0.01	0.02	0.02	0.02	0.02	0.02	0.02
										24-Hour ^d	ı	0.10	0.10	0.11	0.13	0.13	0.14	0.15	0.15	0.16
NO _x	72.00	68.06	64.32	57.00	54.10	52.00	45.22	43.22	42.11	Annual ^c	:	0.12	0.11	0.11	0.11	0.11	0.11	0.11	0.10	0.10
•										1-Hour ^d	ı	2.21	2.13	2.09	2.22	2.13	2.09	2.06	1.98	1.91
со	35.00	33.41	31.33	28.16	26.00	24.22	23.00	22.00	22.00	8-Hour ^c		1.01	0.98	0.95	1.02	0.95	0.91	0.97	0.93	0.92
										1-Hour ^c		1.26	1.22	1.19	1.26	1.18	1.12	1.18	1.13	1.12

^a Concentrations are based on highest predicted concentrations from AERMOD using five years of meteorological data for 2006 to 2010 consisting of surface and upper air data from the National Weather Service stations at Fort Lauderdale-Hollywood Int'l AP and Florida International University (FIU) in Miami.



b Pollutant concentrations were based on a modeled or generic concentration predicted using a modeled emission rate of 79.37 lb/hr (10 g/s) for 5 CTs. Pollutant-specific concentrations for 1 CT were then determined by multiplying the predicted concentration by the ratio of the pollutant-specific emission rate divided by the modeled emission rate of 10 g/s.

^c Based on the highest concentration of any year (2006-2010).

^d Based on highest 5-year average concentration (2006-2010).

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Table 6-5b: Maximum Concentrations Predicted for Emissions of One CT Firing ULSD Oil in Simple-Cycle Operation, Lauderdale (GE 7FA.05 Units)

		Maximum	Emission R	ates for CT	(lb/hr) by O	perating Lo	ad and Air T	emperature	e			Maximum P	redicted Conc	entrations μο	/m³) for CT b	y Operating I	Load and Air	Tem <u>p</u> erature	<u>, a</u>
		Base Load			75% Load			50% Load		Averaging		Base Load			75% Load			50 <u>%</u> Load	
	35°F	75°F	95°	35°F	75°F	95°	35°F	75°F	95°	Time	35°F	75°F	95°	35°F	75°F	95°	35°F	75°F	95°
Generic ^b	79.37	79.37	79.37	79.37	79.37	79.37	79.37	79.37	79.37	Annual ^c	0.14	0.13	0.13	0.16	0.16	0.16	0.19	0.19	0.20
(10 g/s) - 2 g/	/s/CT									Annual ^d	0.10	0.09	0.09	0.12	0.12	0.12	0.14	0.14	0.14
										24-Hour ^c	1.06	1.01	1.04	1.29	1.26	1.29	1.53	1.52	1.54
										24-Hour d	0.81	0.77	0.80	1.00	0.98	1.00	1.20	1.19	1.21
										8-Hour ^c	2.40	2.29	2.37	2.93	2.87	2.93	3.47	3.45	3.50
										3-Hour ^c	2.71	2.60	2.67	3.24	3.19	3.25	3.80	3.78	3.84
										1-Hour ^c	3.00	2.87	2.96	3.61	3.55	3.61	4.22	4.19	4.25
										1-Hour ^d	2.57	2.45	2.53	3.15	3.08	3.15	3.76	3.73	3.79
Emissions for																			
PM ₁₀	37.1	37.1	37.1	37.1	37.1	37.1	37.1	37.1	37.1	Annual ^c	0.06	0.06	0.06	0.08	0.07	0.08	0.09	0.09	0.09
										24-Hour ^c	0.50	0.47	0.49	0.60	0.59	0.60	0.72	0.71	0.72
PM _{2.5}	37.1	37.1	37.1	37.1	37.1	37.1	37.1	37.1	37.1	Annual ^d	0.04	0.04	0.04	0.06	0.05	0.06	0.07	0.07	0.07
										24-Hour d	0.38	0.36	0.37	0.47	0.46	0.47	0.56	0.56	0.57
NO _x	370.3	369.9	349.4	295.1	291.9	277.2	229.5	224.1	213.6	Annual ^c	0.63	0.60	0.59	0.60	0.59	0.57	0.56	0.54	0.53
										1-Hour d	12.00	11.42	11.14	11.71	11.34	11.00	10.87	10.54	10.20
со	71.0	73.0	70.0	58.0	56.3	54.2	46.4	46.3	45.3	8-Hour ^c	2.15	2.11	2.09	2.14	2.03	2.00	2.03	2.01	2.00
										1-Hour c	2.69	2.64	2.61	2.64	2.52	2.47	2.47	2.45	2.42

^a Concentrations are based on highest predicted concentrations from AERMOD using five years of meteorological data for 2006 to 2010 consisting of surface and upper air data from the National Weather Service stations at Fort Lauderdale-Hollywood Int'l AP and Florida International University (FIU) in Miami.



^b Pollutant concentrations were based on a modeled or generic concentration predicted using a modeled emission rate of 79.37 lb/hr (10 g/s) for 5 CTs. Pollutant-specific concentrations for 1 CT were then determined by multiplying the predicted concentration by the ratio of the pollutant-specific emission rate divided by the modeled emission rate of 10 g/s.

^c Based on the highest concentration of any year (2006-2010).

^d Based on highest 5-year average concentration (2006-2010).



Table 6-6a: Maximum Concentrations Predicted for Emission of One CT Firing Natural Gas in Simple-Cycle Operation, Lauderdale (Siemens F5 Units)

	Maximum	Emission F	Rates for CT Tempe		perating L	oad and Air		 aximum P	redicted Cor	ncentrations (Air Temp		by Operati	ng Load an
		Base Load		40%	Load	44% Load	Averaging		Base Load		40%	Load	44% Load
	35°F	7 5°F	95°	35°F	7 5°F	95°	Time	35°F	7 5°F	95°	35°F	7 5°F	95°
Generic ^b	79.37	79.37	79.37	79.37	79.37	79.37	Annual ^c	0.13	0.12	0.12	0.20	0.20	0.19
(10 g/s)							Annual d	0.09	0.08	0.09	0.15	0.14	0.14
							24-Hour ^c	1.00	0.92	0.97	1.58	1.55	1.53
							24-Hour d	0.76	0.70	0.74	1.24	1.21	1.20
							8-Hour ^c	2.26	2.08	2.19	3.57	3.51	3.47
							3-Hour ^c	2.56	2.37	2.49	3.91	3.84	3.80
							1-Hour °	2.83	2.61	2.75	4.32	4.25	4.21
							1-Hour d	2.41	2.21	2.34	3.87	3.80	3.75
Emissions r	epresent one	<u>CT</u>											
PM ₁₀	9.0	10.0	9.0	8.0	8.0	8.0	Annual ^c	0.014	0.015	0.014	0.020	0.020	0.020
							24-Hour °	0.11	0.12	0.11	0.159	0.156	0.154
PM _{2.5}	9.0	10.0	9.0	8.0	8.0	8.0	Annual d	0.010	0.010	0.010	0.015	0.015	0.014
							24-Hour d	0.09	0.09	0.08	0.12	0.12	0.12
NO_x	77.0	79.0	74.0	42.0	42.0	42.0	Annual ^c	0.1233	0.117	0.115	0.106	0.104	0.103
							1-Hour d	2.34	2.20	2.18	2.05	2.01	1.99
СО	21.0	21.0	20.0	26.0	26.0	26.0	8-Hour °	0.5971	0.5505	0.5520	1.1704	1.1491	1,1360
							1-Hour ^c	0.7481	0.6918	0.6925	1.4154	1.3931	1.3792

^a Concentrations are based on highest predicted concentrations from AERMOD using five years of meteorological data for 2006 to 2010 consisting of surface and upper air data from the National Weather Service stations at Fort Lauderdale-Hollywood Int'l AP and Florida International University (FIU) in Miami.



^b Pollutant concentrations were based on a modeled or generic concentration predicted using a modeled emission rate of 79.37 lb/hr (10 g/s) for 5 CTs. Pollutant-specific concentrations for 1 CT were then determined by multiplying the predicted concentration the ratio of the pollutant-specific emission rate divided by the modeled emission rate of 10 g/s.

^c Based on the highest concentration of any year (2006-2010).

^d Based on highest 5-year average concentration (2006-2010).



Table 6-6b: Maximum Concentrations Predicted for Emissions of One CT Firing ULSD Oil in Simple-Cycle Operation, Lauderdale (Siemens F5 Units)

	Maximum	Emission F	tates for C1	(lb/hr) by Op erature	erating Lo	ad and Air			- IVIAXIIII III I		ncentrations (Air Temp	. • .	by Operating	J LOAU ai
		Base Load			50% Load		Averaging			Base Load			50% Load	
_	35°F	75°F	95°	35°F	75°F	95°	Time		35°F	7 5°F	95°	35°F	75°F	95°
Seneric ^b	79.37	79.37	79.37	79.37	79.37	79.37	Annual	C	0.13	0.12	0.13	0.18	0.18	0.19
10 g/s) - 2 g/	/s/CT						Annual	ď	0.09	0.09	0.09	0.13	0.13	0.14
							24-Hour	С	0.99	0.95	1.00	1.44	1.43	1.46
							24-Hour	ď	0.75	0.72	0.76	1.12	1.11	1.14
							8-Hour	c	2.23	2.16	2.27	3.26	3.24	3.32
							3-Hour	c	2.53	2.45	2.57	3.58	3.56	3.64
							1-Hour	С	2.80	2.71	2.84	3.99	3.96	4.05
							1-Hour	ď	2.38	2.30	2.42	3.53	3.50	3.59
<u>missions re</u>	present that o	of one CT												
PM ₁₀	53.0	52.0	48.0	37.0	35.0	33.0	Annual	С	0.08	0.08	80.0	0.08	0.08	0.08
							24-Hour	С	0.66	0.62	0.61	0.67	0.63	0.61
PM _{2.5}	53.0	52.0	48.0	37.0	35.0	33.0	Annual	d	0.06	0.06	0.05	0.06	0.06	0.06
							24-Hour	d	0.50	0.47	0.46	0.52	0.49	0.47
NO _x	378.0	376.0	353.0	235.0	228.0	217.0	Annual	с	0.60	0.58	0.57	0.54	0.52	0.51
							1-Hour	ď	11.35	10.89	10.76	10.44	10.06	9.82
со	49.0	49.0	46.0	340.0	331.0	315.0	8-Hour	с	1.38	1.33	1.31	13.98	13.52	13.1
							1-Hour	С	1.73	1.67	1.65	17.08	16.53	16.0

^a Concentrations are based on highest predicted concentrations from AERMOD using five years of meteorological data for 2006 to 2010 consisting of surface and upper air data from the National Weather Service stations at Fort Lauderdale-Hollywood International Airport and Florida International University (FIU) in Miami.



^b Pollutant concentrations were based on a modeled or generic concentration predicted using a modeled emission rate of 79.37 lb/hr (10 g/s) for 5 CTs. Pollutant-specific concentrations for 1 CT were then determined by multiplying the predicted concentration by the ratio of the pollutant-specific emission rate divided by the modeled emission rate of 10 g/s.

^c Based on the highest concentration of any year (2006-2010).

^d Based on highest 5-year average concentration (2006-2010).





Table 6-7: Summary of Maximum Pollutant Concentrations Predicted for Natural Gas and ULSD Oil Firing, Lauderdale (5 GE7FA.0

	Averaging	Concentra	tions (µg/m3)	EPA Class II Significant
Pollutant	Time	Natural Gas Limited to 3390 hrs/yr	Max. 2,890 hrs/yr Natural Gas & Max. 500 Hrs/Yr ULSD Oil ^a	lmpact Levels (μg/m3)
PM ₁₀	Annual	0.05	0.07	1
10	24-Hour	0.99	1.75	5
PM _{2.5}	Annual	0.04	0.05	0.3
	24-Hour	0.77	1.63	1.2
Tier 1				
NO ₂	Annual	0.23	0.37	1
Tier 2 ^b	1-Hour	11.1	60.0	7.52
NO ₂	Annual	0.17	0.28	1
	1-Hour	8.9	48.0	7.52
СО	8-Hour	5.1	10.8	500
	1-Hour	6.3	13.4	2,000

Maximum Hours of Fuel Usage

Natural Gas 3,390 Fuel Oil 500



^a Maximum 24-hour impacts based on 10 hours on fuel oil firing and 14 hours of natural gas firing.

^b Assumes 75% conversion of NO_x to NO₂ for annual and 80% converstion of NO_x to NO₂ for 1-hour.





Table 6-8: Summary of Maximum Pollutant Concentrations Predicted for Natural Gas and ULSD Oil Firing, Lauderdale (5 Siemens F5 Units)

	Averaging	Concent	EPA Class II Significant		
Pollutant	Time	Natural Gas Limited to 3,390 hrs/yr	Max. 2890 Hrs/Yr Natural Gas & Max. 500 hrs/yr ULSD Oil ^a	lmpact Levels (μg/m3)	
PM ₁₀	Annual	0.04	0.06	1	
	24-Hour	0.79	1.86	5	
PM _{2.5}	Annual	0.03	0.04	0.3	
	24-Hour	0.62	1.45	1.2	
Tier 1					
NO ₂	Annual	0.24	0.37	1	
	1-Hour	11.7	56.8	7.52	
Tier 2 ^b					
NO ₂	Annual	0.18	0.28	1	
	1-Hour	9.3	45.4	7.52	
со	8-Hour	5.9	69.9	500	
	1-Hour	7.1	85.4	2,000	

Maximum Hours of Fuel Usage

Natural Gas 3,390 Fuel Oil 500



^a Maximum 24-hour impacts based on 10 hours on ULSD oil firing and 14 hours of natural gas firing. ^b Assumes 75% conversion of NO_x to NO_2 for annual and 80% conversion of NO_x to NO_2 for 1-hour.





Table 6-9: Maximum Predicted 1-hour NO₂ and 24-hour PM_{2.5} Impacts Compared to the NAAQS

CT Type, Pollutant,	Maximur	n Concentrati	on (µg/m³)	Receptor	r Location	
Averaging Time and Rank	Total	Modeled Sources ^a	Background	UTM- East (m)	UTM- North (m)	AAQS (µg/m³)
Siemens CTs NO ₂ ^a						
1-Hour, 98th Percentile	167.7	82.4	85.3	579,040	2,883,670	188.1
PM _{2.5} 24-Hour, 98th Percentile	17.8	3.2	14.6	579,040	2,883,420	35
GE7FA.05 CTs NO ₂ ^a						
1-Hour, 98th Percentile	167.7	82.4	85.3	579,040	2,883,670	. 188.1
PM _{2.5} 24-Hour, 98th Percentile	17.7	3.1	14.6	579,040	2,883,420	35

Concentrations are based on concentrations predicted using 5 years of meteorological data from 2006 to 2010 of surface and upper air data from the National Weather Service stations at Fort Lauderdale/Hollywood International Airport and Miami, FL, respectively.



^a A NO_X to NO₂ converstion factor of 80% applies based on EPA's Guidline on Air Quality Models Tier 2 approach.



Table 6-10: Maximum Predicted 24-hour PM_{2.5} Impact from all PSD Sources Compared to the Allowable PSD Class II Increment

Averaging Time and Rank	Maximum Concentration ^a (μg/m ³)	Receptor UTM- East (m)	r Location UTM- North (m)	Allowable PSD Class II Increment (µg/m³)
Siemens F5 CTs 24-HR, H2H	2.0	579,540	2,884,170	9
<u>GE7FA.05 CTs</u> 24-HR, H2H	1.5	579,540	2,884,170	9

H2H = Highest, Second Highest



Concentrations are predicted using 5 years of meteorological data from 2006 to 2010 with surface and upper air data from the National Weather Service stations at Fort Lauderdale/Hollywood International Airport and Miami, FL, respectively.

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Table 6-11: Maximum Pollutant Concentrations at the ENP Compared to the PSD Class I Area SIL

Pollutant	Averaging		ncentrations ^a a	t EN			- 00	D Class I CII
	Time		A.05 CTs	_		ens F5	- PS	D Class I SIL
		3,390 hrs on Nat.Gas	2,890 hrs Nat Gas & 500 Hrs Oil		3,390 hrs on Nat.Gas	2,890 hrs Nat Gas & 500 Hrs Oil		(μg/m³)
NO ₂	Annual	0.006	0.009	b	0.005	0.008	b	0.1
	24-Hour	0.35	1.82	С	0.38	1.85	С	
	8-Hour	0.88	4.47		0.98	4.66		
	3-Hour	1.14	6.13		1.19	6.00		
	1-Hour	1.33	7.09		1.54	7.180		
PM ₁₀	Annual	0.002	0.002	b	0.002	0.002	b	0.2
	24-Hour	0.08	0.27	С	0.07	0.38	С	0.3
	8-Hour	0.19	0.65		0.18	0.95		
	3-Hour	0.25	0.90		0.22	1.24		
	1-Hour	0.33	1.19		0.32	1.661		
PM _{2.5}	Annual	0.002	0.002	b	0.002	0.002	b	0.06
	24-Hour	0.08	0.27	С	0.07	0.38	С	0.07
	8-Hour	0.19	0.65		0.18	0.95		
	3-Hour	0.25	0.90		0.22	1.24		
	1-Hour	0.33	1.19		0.32	1.661		
co	Annual	0.005	0.006	b	0.004	0.004	b	
	24-Hour	0.25	0.52	С	0.19	0.36	С	
	8-Hour	0.63	1.25		0.47	0.88		
	3-Hour	0.83	1.72		0.58	1.15		
	1-Hour	1.10	2.29		0.84	1.541		

SIL = Class I Significant Impact Level



^a Concentrations are based on highest predicted concentrations from CALPUFF v5.8 using 3 years of meteorological data for 200

^b Annual concentrations based on 500 hours of fuel oil and 2890 hours of natural gas firing

^{° 24-}hour concentrations based on 10 hours of fuel oil and 14 hours of natural gas firing.

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Examples of Reported Effects of Air Pollutants at Concentrations Below National Secondary Ambient Air Quality Standards

Pollutant	Reported Effect	Concentration (μg/m³)	Exposure
Nitrogen Dioxide ^{b,c}	Respiratory stress in mice Respiratory stress in guinea pigs	1,917 96 to 958	3 hours 8 hours/day for 122 days
Particulates ^a	Respiratory stress, reduced respiratory disease defenses	120 PbO ₃	continually for 2 months
	Decreased respiratory disease defenses in rats, same with hamsters	100 NiCl₂	2 hours

Sources:

 ^a Newman and Schreiber, 1988.
 ^b Gardner and Graham, 1976.
 ^c Trzeciak et al., 1977.





Table 7-2: Maximum 24-Hour Visibility Impairment Predicted for the Project at the ENP PSD Class I Area

Visibil	Visibility Impairment		
2001	2002	2003	Criteria (deciview)
0.13	0.17	0.18	0.5
0.13	0.18	0.18	0.5
0.46	0.66	0.46	0.5
0.49	0.72	0.67	0.5
0.27	0.37	0.30	0.5
0.28	0.41	0.38	0.5
	0.13 0.13 0.46 0.49	2001 2002 0.13 0.17 0.13 0.18 0.46 0.66 0.49 0.72 0.27 0.37	0.13 0.17 0.18 0.13 0.18 0.18 0.46 0.66 0.46 0.49 0.72 0.67 0.27 0.37 0.30

SC CTs = Simple Cycle Combustion Turbines



^a Values presented are 98th-percentile deciviews using CALPUFF v5.8 and CALPOST v6.221, MVISBK=8, M8_MODE=5. Background extinctions are based on FLAG 2008 and 20th best natural background values.



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Table 7-3: Maximum Annual Total Sulfur and Nitrogen Deposition Predicted for the Project at the ENP PSD Class | Area

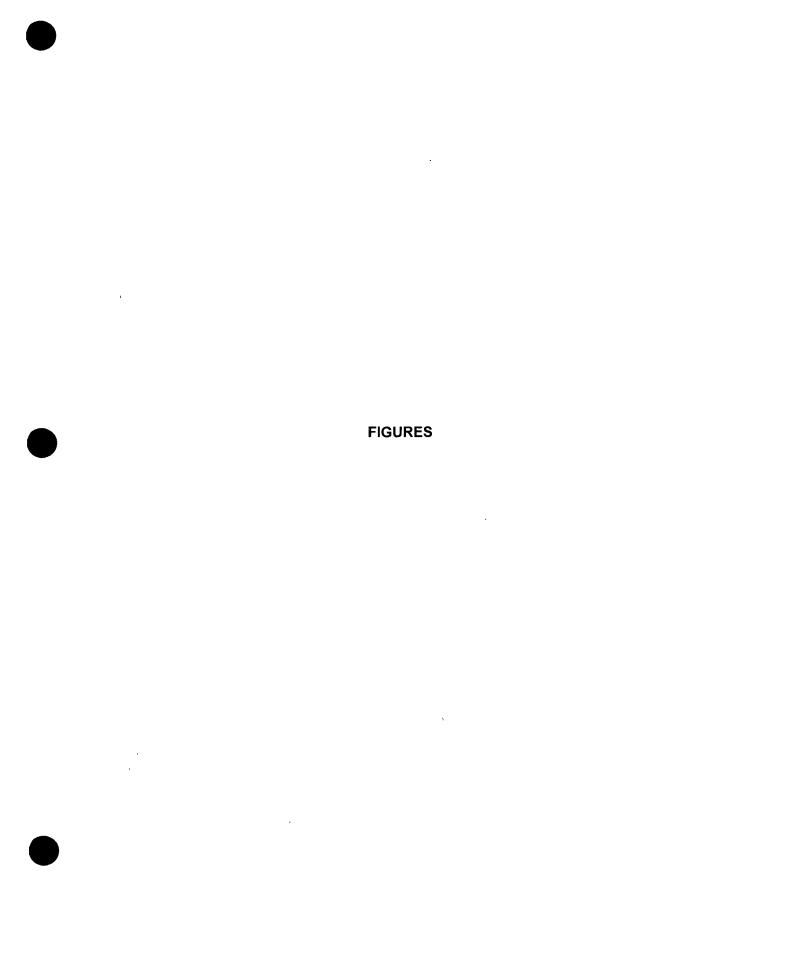
	Total Deposit	ion (Wet & Dry)		Deposition Analysis Threshold ^b	
CT Configuration/Species	(g/m²/s)	(kg/ha/yr) ^{a,c}	Year	(kg/ha/yr)	
5 GE 7FA.05 SC CTs					
	7.79E-12	0.0025	2001	0.01	
	8.51E-12	0.0027	2002	0.01	
	1.11E-11	0.0035	2003	0.01	
5 Siemens F5 SC CTs		,			
	8.03E-12	0.0025	2001	0.01	
	8.71E-12	0.0027	2002	0.01	
	1.13E-11	0.0036	2003	0.01	

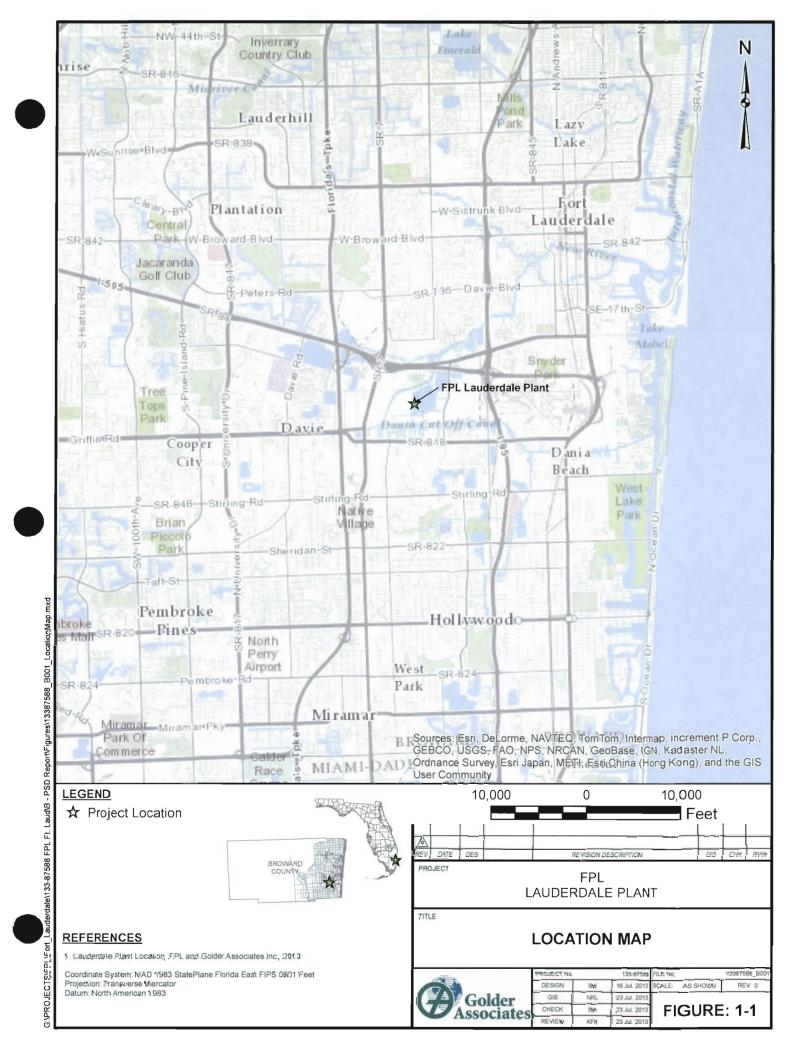
^a Conversion factor is used to convert g/m²/s to kg/hectare (ha)/yr with the following units:

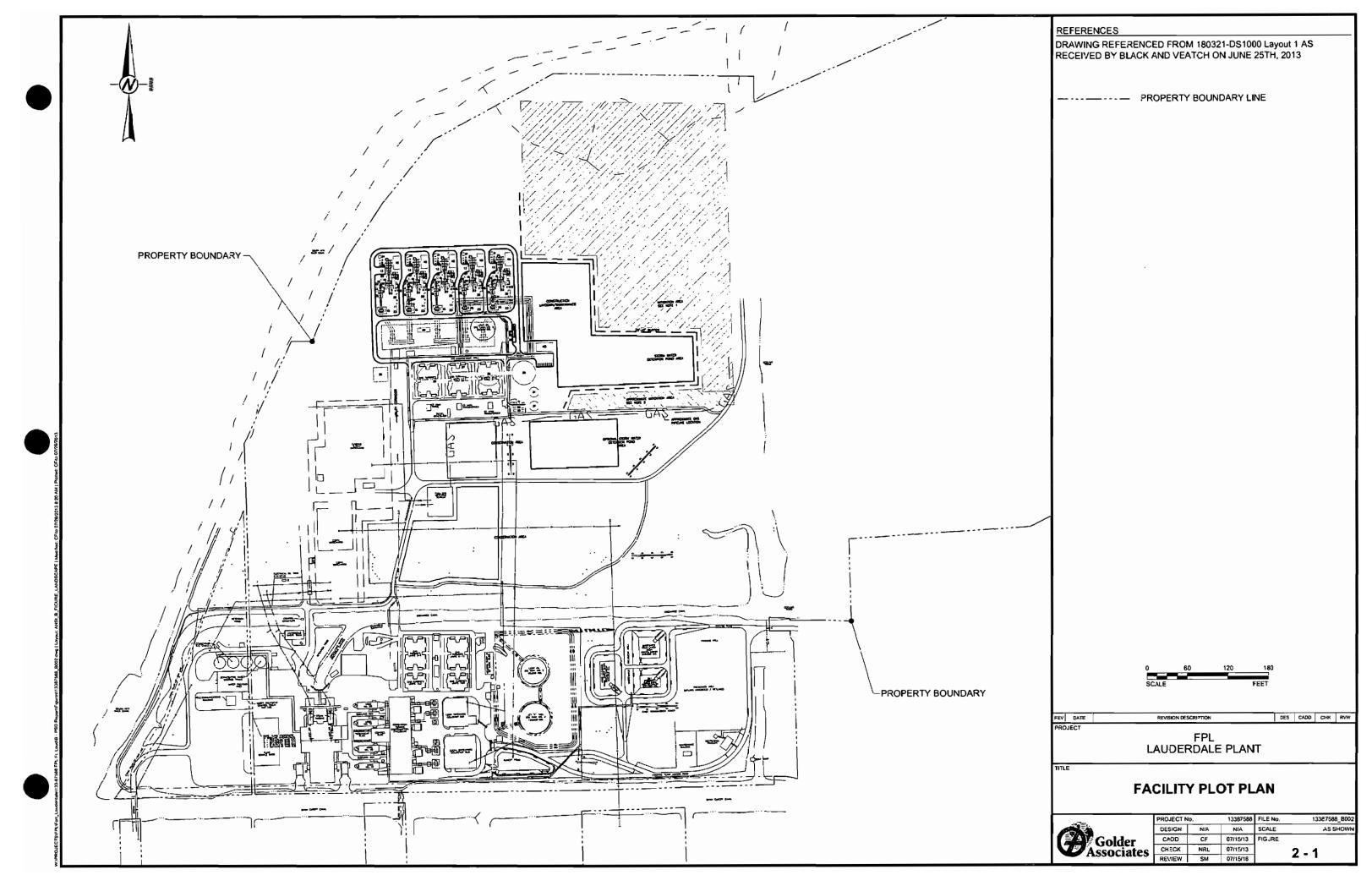


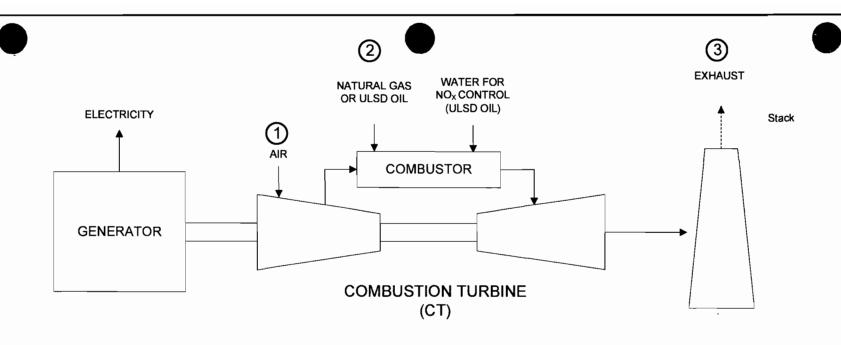
Deposition analysis thresholds (DAT) for nitrogen deposition provided by the U.S. Fish and Wildlife Service, January 2002. A DAT is the additional amount of nitrogen or sulfur deposition within a Class I area, below which estimated impacts from a propsed new or modified source are considered insignificant.

^c Total nitrogen deposition is based on CTs operating 2890 hr/yr on natural gas and 500 hr/yron ULSD oil









	Parameters	Units	Fuel	GE 7FA.05	Siemens F5
①	Inlet Air (at 75°F)	lb/hr	Gas	4,130,000	4,576,438
		lb/hr	Oil	4,198,000	4,649,675
2	CT Heat Input	MMBtu/hr (HHV)	Gas	2,090	2,297
•		MMBtu/hr (HHV)	Oil	2,260	2,193
3	Stack Velocity	ft/sec	Gas	112.6	124
		ft/sec	Oil	114	121.5
3	Stack Temperature	°F	Gas	1,117	1,108
<u></u>		°F	Oil	1,106	1,067
3	Stack Height	feet	Gas/Oil	80	80
3	Stack Diameter	feet	Gas/Oil	23	23

Figure 2-2. Process Flow Diagram for Each CT Baseload Operation, Turbine Inlet Temperature of 75°F FPL Lauderdale CT Project, Broward County, Florida

Source: GE, 2013; Siemens, 2013; Golder, 2013.

Process Flow Legend
Solid/Liquid
Gas
Steam

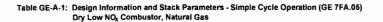


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APPENDIX A

EXPECTED PERFORMANCE AND EMISSION INFORMATION FOR GE 7FA.05 CTS AND GE 7FA.04 CTS





					CT Only				
		l Turbine Intet Te			Turbine Inlet Te			Turbine Inlet Te	
Parameter	35° F	75° F	95° F	35° F	75° F	95° F	35° F	75° F	95° F
Combustion Turbine Performance									
Heat Input (MMBtu/hr, LHV)	1,990.3	1,883.1	1,779.0	1,570.1	1,497.0	1,430.9	1,250.6	1,196.3	1,166.1
Heat Input (MMBtu/hr, HHV)	2,209.2	2,090.2	1,974.7	1,742.8	1,661.7	1,588.3	1,388.2	1,327.9	1,294.4
Evaporative Cooler	None	None	None	None	None	None	None	None	None
Relative Humidity (%)	60	60	60	60	60	60	60	60	60
Fuel heating value (Btu/lb, LHV)	21,515	21,515	21,515	21,515	21,515	21,515	21,515	21,515	21,515
Fuel heating value (Btu/lb, HHV)	23,879	23,879	23,879	23,879	23,879	23,879	23,879	23,879	23,879
Ratio of fuel heating values (HHV/LHV)	1.110	1.110	1.110	1.110	1.110	1.110	1.110	1.110	1.110
CT Exhaust Flow									
olume flow (acfm) = [Mass flow (lb/hr) x 1545.4 x									
Mass Flow (lb/hr)	4,278,000	4,130,000	3,913,000	3,450,000	3,208,000	3,033,000	2,758,000	2,704,000	2,712,000
Temperature (°F)	1,098	1,117	1,132	1,109	1,174	1,209	1,202	1,215	1,215
Moisture (% Vol.)	8.05	9.16	10.62	7.89	9.34	10.89	7.87	8.95	10.23
Oxygen (% Vol.)	12.40	12.34	12.09	12.58	12.15	11.79	12.61	12.58	12.53
Molecular Weight	28.42	28.30	28.13	28.44	28.29	28.12	28.44	28.31	28.16
Volume flow (acfm)	2,859,044	2,806,249	2,699,692	2,320,884	2,259,352	2,195,150	1,965,032	1,950,402	1,966,615
Fuel Usage									
Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000									
Heat Input (MMBtu/hr, LHV)	1,990.3	1,883.1	1,779.0	1,570.1	1,497.0	1,430.9	1,250.6	1,196.3	1,166.1
Heat Content (Btu/lb, LHV)	21,515	21,515	21,515	21,515	21,515	21,515	21,515	21,515	21,515
Fuel Usage (lb/hr)	92,508	87,525	82,686	72,977	69,579	66,507	58,127	55,603	54,199
Heat Content (Btu/cf, LHV)	918	918	918	918	918	918	918	918	918
Fuel Density (lb/ft ³)	0.0427	0.0427	0.0427	0.0427	0.0427	0.0427	0.0427	0.0427	0.0427
Fuel Usage (cf/hr)	2,168,083	2,051,307	1,937,908	1,710,349	1,630,719	1,558,715	1,362,309	1,303,159	1,270,261
CT Stack Parameters									
Stack Height (feet)	80	80	80	80	80	80	80	80	80
Stack Diameter (feet)	23	23	23	23	23	23	23	23	23
CT Stack Flow Conditions									
	')2 /4) x 3.14159] / 60 se								
			1,132	1,109	1,174	1,209	1,202	1,215	1,215
Stack Temperature (°F)	1,098	1,117							
Velocity (fl/sec) = Volume flow (acfm) / [((diameter Stack Temperature (°F) Volume flow (acfm)	2,859,044	2,806,249	2,699,692	2,320,884	2,259,352	2,195,150	1,965,032	1,950,402	1,966,615
Stack Temperature (°F)					2,259,352 23	2,195,150 23	1,965,032 23	1,950,402 23 78.2	1,966,615 23 78.9

Note: Universal gas constant = 1,545.4 ft-lb(force)/°R; atmospheric pressure = 2,112.5 lb(force)/ft² (@14.67 psia).







Table GE-A-2: Maximum Emissions for Criteria Pollutants - Simple Cycle Operation (GE 7FA.05) Dry Low $NO_{\rm X}$ Combustor, Natural Gas, Base Load

					CT Only				
B		Turbine Inlet T			urbine Inlet To			Turbine Inlet To	
Parameter	35° F	/5° F	95° F	35° F	75° F	95° F	35° F	75° F	95° F
Particulate Matter (PM10/PM2.5)									
PM 10/PM 25 (lb/hr) = PM 10 Emissions Rate (lb/MMBtu)	x Heat Input (MMBtu/hr, F	IHV) (front-half	& back-half)						
PM ₁₀ Emission Rate (lb/MMBtu, HHV)	0.00480	0.00507	0.00537	0.00608	0.00638	0.00667	0.00764	0.00798	0.00819
Heat Input (MMBtu/hr, HHV)	2.209.2	2.090.2	1.974.7	1.742.8	1.661 7	1.588.3	1.388.2	1.327.9	1.294.4
PM ₁₀ /PM _{2.5} Emission Rate (lb/hr)	10.6	10.6	10.6	10.6	10.6	10.6	10.6	10.6	10.6
, ,	NA	9.4	NA	NA	NA	NA	NA	NA	NA
Sulfur Dioxide (SO ₂)									
SO 2 (lb/hr)= Natural gas (scf/hr) x sulfur content(gr/100	scf) x 1 lb/7000 gr x (lb S	O 2 /b S) /100							
Fuel Use (scf/hr)	2,168,083	2,051,307	1,937,908	1,710,349	1,630,719	1,558,715	1,362,309	1,303,159	1,270,261
Sulfur Content (grains/ 100 cf)	2	2	2	2	2	2	2	2	2
lb SO ₂ /lb S (64/32)	2	2	2	2	2	2	2	2	2
SO ₂ Emission Rate (lb/hr)	12.4	11.7	11.1	9.8	9.3	8.9	7.8	7.4	7.3
SO 2 (lb/hr)= SO 2 Emissions Rate (lb/MMBtu) x Heat In	put (MMBtu/hr, HHV)								
SO ₂ Emission Rate (lb/MMBlu)	0.0060	0.0060	0.0060	0.0060	0.0060	0.0060	0.0060	0.0060	0.0060
Heat Input (MMBtu/hr, HHV)	2,209.2	2,090.2	1,974.7	1,742.8	1,661.7	1,588.3	1,388.2	1,327.9	1,294.4
SO ₂ Emission Rate (lb/hr)	13.2	12.5	11.8	10.5	10.0	9.5	8.3	8.0	7.8
Nitrogen Oxides (No.)									
NO_x (ppmv actual) = NO_x (ppmd @ 15%O ₂) x [(20.9 -	O 2 dry)/(20.9 - 15)] x [1-	Moisture(%)/10	00]						
Oxygen (%, dry)(O 2 dry) = Oxygen (%)/[1-Moisure (%)]			-						
NO, $(lb/hr) = NO$, $(ppm actual) \times Volume flow (acfm) x$						(0000 60	_		
$NU_{+}(ID/NF) = NU_{+}(DDM actual) \times Volume flow (actm) X$	46 (mole, wat NO ,) x 21	12.5 lb/ft" (pres	(Sure) / (1545.4 f	l-lb (gas constan	it. R) x Actual T	emp. ("R)) x ov i	nın/hr		
NO_x (lb/nr) $\approx NO_x$ (ppm actual) x volume now (acm) x Basis, ppm actual	46 (mole. wgt NO _x) x 21: 10 4	12.5 lb/ft" (pres 10.1	sure) / [1545.4 fi 10.1	t-lb (gas constan 10.2	nt, R) x Actual Ti 10.4	emp. (*R) j x ou i 10.4	<i>min/hr</i> 10.1	9.8	9.5
Basis, ppm actual								9.8 9.0	9.5 9.0
	10 4	10.1	10.1	10.2	10.4	10.4	10.1		
Basis, ppm actual NO _x , ppmvd @15% O ₂ (15 ppmvd)	10 4 9.0	10.1 9.0	10.1 9.0	10.2 9.0	10.4 9.0	10.4 9.0	10.1 9.0	9.0	9.0
Basis, ppm actual NO _x , ppmvd @15% O ₂ (15 ppmvd) Moisture (%)	10 4 9.0 8,05	10.1 9.0 9.16	10.1 9.0 10.62	10.2 9.0 7.89	10.4 9.0 9.34	10.4 9.0 10.89	10.1 9.0 7.87	9.0 8.95	9.0 10.23 12.53 13.96
Basis, ppm actual NO _n , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%)	10 4 9.0 8.05 12.40	10.1 9.0 9.16 12.34	10.1 9.0 10.62 12.09	10.2 9.0 7.89 12.58	10.4 9.0 9.34 12.15	10.4 9.0 10.89 11.79	10.1 9.0 7.87 12.61	9.0 8.95 12.58	9.0 10.23 12.53 13.96
Basis, ppm actual NO _n , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) dry	10 4 9.0 8.05 12.40 13.49 2.859,044 2.628,891	10.1 9.0 9.16 12.34 13.58 2,806,249 2,549,197	10.1 9.0 10.62 12.09 13.53 2,699,692 2,412,985	10.2 9.0 7.89 12.58 13.66 2,320,884 2,137,766	10.4 9.0 9.34 12.15 13.40 2,259,352 2,048,329	10.4 9.0 10.89 11.79 13.23 2,195,150 1,956,098	10.1 9.0 7.87 12.61 13.69 1,965,032 1,810,384	9.0 8.95 12.58 13.82 1.950,402 1,775,841	9.0 10.23 12.53 13.96 1,966,613 1,765,43
Basis, ppm actual NO _n , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) for ppmvd (acfm)	10 4 9.0 8.05 12.40 13.49 2.859,044 2.628,891 1,098	10.1 9.0 9.16 12.34 13.58 2,806,249 2,549,197 1,117	10.1 9.0 10.62 12.09 13.53 2,699,692 2,412,985 1,132	10.2 9.0 7.89 12.58 13.66 2,320,884 2,137,766 1,109	10.4 9.0 9.34 12.15 13.40 2,259,352 2,048,329 1,174	10.4 9.0 10.89 11.79 13.23 2,195,150 1,956,098 1,209	10.1 9.0 7.87 12.61 13.69 1,965,032 1,810,384 1,202	9.0 8.95 12.58 13.82 1.950,402 1,775,841 1,215	9.0 10.23 12.53 13.96 1,966,619 1,765,43 1,215
Basis, ppm actual NO _n , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) Flow (acfm) Flow (acfm), dry	10 4 9.0 8.05 12.40 13.49 2.859,044 2.628,891	10.1 9.0 9.16 12.34 13.58 2,806,249 2,549,197	10.1 9.0 10.62 12.09 13.53 2,699,692 2,412,985	10.2 9.0 7.89 12.58 13.66 2,320,884 2,137,766	10.4 9.0 9.34 12.15 13.40 2,259,352 2,048,329 1,174 54.1	10.4 9.0 10.89 11.79 13.23 2,195,150 1,956,098	10.1 9.0 7.87 12.61 13.69 1,965,032 1,810,384 1,202 45.2	9.0 8.95 12.58 13.82 1.950,402 1,775,841	9.0 10.23 12.53 13.96 1,966,618 1,765,43 1,215 42.1
Basis, ppm actual NO _n , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) Oxygen (%) Flow (acfm) Flow (acfm), dry Exhaust Temperature (*F) NO _x Emission Rate (lb/hr)	10 4 9.0 8.05 12.40 13.49 2.859,044 2.628,891 1,098 72.0 72.0	10.1 9.0 9.16 12.34 13.58 2,806,249 2,549,197 1,117	10.1 9.0 10.62 12.09 13.53 2,699,692 2,412,985 1,132	10.2 9.0 7.89 12.58 13.66 2,320,884 2,137,766 1,109	10.4 9.0 9.34 12.15 13.40 2,259,352 2,048,329 1,174	10.4 9.0 10.89 11.79 13.23 2,195,150 1,956,098 1,209	10.1 9.0 7.87 12.61 13.69 1,965,032 1,810,384 1,202	9.0 8.95 12.58 13.82 1.950,402 1,775,841 1,215	9.0 10.23 12.53 13.96 1,966,619 1,765,43 1,215
Basis, ppm actual NO _n , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) Oxygen (%) Flow (acfm) Flow (acfm), dry Exhaust Temperature (*F) NO _x Emission Rate (lb/hr)	10 4 9.0 8.05 12.40 13.49 2.859,044 2.628,891 1,098 72.0 72.0	10.1 9.0 9.16 12.34 13.58 2,806,249 2,549,197 1,117 68.1	10.1 9.0 10.62 12.09 13.53 2,699.692 2,412,985 1,132 64.3	10.2 9.0 7.89 12.58 13.66 2,320,884 2,137,766 1,109 56.8	10.4 9.0 9.34 12.15 13.40 2,259,352 2,048,329 1,174 54.1	10.4 9.0 10.89 11.79 13.23 2,195,150 1,956,098 1,209 51.7	10.1 9.0 7.87 12.61 13.69 1,965,032 1,810,384 1,202 45.2	9.0 8.95 12.58 13.82 1.950,402 1,775,841 1,215 43.2	9.0 10.23 12.53 13.96 1,966,619 1,765,43 1,215 42.1
Basis, ppm actual NO _x , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) NO (acfm) Flow (acfm) Flow (acfm) NO _x Emission Rate (lb/hr)	10 4 9.0 8.05 12.40 13.49 2.859,044 2.628,891 1,098 72.0 72.0	10.1 9.0 9.16 12.34 13.58 2,806,249 2,549,197 1,117 68.1	10.1 9.0 10.62 12.09 13.53 2,699.692 2,412,985 1,132 64.3	10.2 9.0 7.89 12.58 13.66 2,320,884 2,137,766 1,109 56.8	10.4 9.0 9.34 12.15 13.40 2,259,352 2,048,329 1,174 54.1	10.4 9.0 10.89 11.79 13.23 2,195,150 1,956,098 1,209 51.7	10.1 9.0 7.87 12.61 13.69 1,965,032 1,810,384 1,202 45.2	9.0 8.95 12.58 13.82 1.950,402 1,775,841 1,215 43.2	9.0 10.23 12.53 13.96 1,966,615 1,765,43 1,215 42.1 42.0
Basis, ppm actual NO., ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) Oxygen (%) Oxygen (%) Flow (acfm) Flow (acfm), dry Exhaust Temperature (*F) NO., Emission Rate (lb/hr) NO., (lb/hr) = NO., Emissions Rate (lb/MMBtu) x Heat II.	10 4 9.0 8.05 12.40 13.49 2.859,044 2.628,891 1,098 72.0 72.0	10.1 9.0 9.16 12.34 13.58 2,806,249 2,549,197 1,117 68.1 68.0	10.1 9.0 10.62 12.09 13.53 2,699.692 2,412.985 1,132 64.3 64.0	10.2 9.0 7.89 12.58 13.66 2,320,884 2,137,766 1,109 56.8 57.0	10.4 9.0 9.34 12.15 13.40 2,259,352 2,048,329 1,174 54.1 54.0	10.4 9.0 10.89 11.79 13.23 2,195,150 1,956,098 1,209 51.7 52.0	10.1 9.0 7.87 12.61 13.69 1,965,032 1,810,384 1,202 45.2 45.0	9.0 8.95 12.58 13.82 1.950,402 1,775,841 1,215 43.2 43.0	9.0 10.23 12.53 13.96 1,966,618 1,765,43 1,215 42.1







Table GE-A-2: Maximum Emissions for Criteria Pollutants - Simple Cycle Operation (GE 7FA.05) Dry Low ${\rm NO_X}$ Combustor, Natural Gas, Base Load

	<u></u>				CT Only				
_		Turbine inlet T			Turbine Infet T			Furbine Inlet Te	
Parameter	35° F	75° F	95° F	35° F	75° F	95° F	35° F	75° F	95° F
Carbon Monoxide (CO)									
CO (ppmv wet or actual) = CO (ppmvd @ 15%O 2) x [(20.9 - O , dry)/(20.9 - 15)]	x [1- Moisture(%	6)/1001						
Oxygen (%, dry)(O 2 dry) = Oxygen (%)/[1-Moisure (%		•							
CO (lb/hr) = CO (ppm actual) x Volume flow (acfm) x 2		lh/ft² (pressure) / [1545 4 ff_lh (nas constant Ri	y Actual Temp	(°R)1 x 60 min/h	r		
Basis, ppm actual	8.28	8.18	8.04	8.29	8.16	8.02	8.29	8.19	8.08
Basis, ppmvd	9.0	9.0	9.0	9.0	9.0	9.0	9.0	9.0	9.0
Basis, ppmvd @ 15% O ₂	7.16	7.26	7.20	7.33	7.08	6.92	7.36	7.50	7.65
Moisture (%)	8.05	9 16	10.62	7.89	9.34	10.89	7.87	8.95	10.23
Oxygen (%)	12 40	12.34	12.09	12.58	12.15	11.79	12.61	12.58	12.53
Oxygen (%) dry	13 49	13.58	13.53	13.66	13.40	13.23	13.69	13.82	13.96
Flow (acfm)	2.859.044	2.806.249	2.699.692	2.320.884	2.259.352	2.195.150	1.965.032	1.950.402	1,966,615
Flow (acfm), dry	2,628,891	2,549,197	2,412,985	2,137,766	2,048,329	1,956,098	1,810,384	1,775,841	1,765,43
Exhaust Temperature (°F)	1.098	1,117	1,132	1,109	1.174	1.209	1,202	1,215	1,215
CO Emission Rate (lb/hr)	34.9	33.4	31.3	28.2	25.9	24.2	22.5	21.9	21.8
	35.0	33.0	31.0	28.0	26.0	24.0	23.0	22.0	22.0
CO (lb/hr) = CO Emissions Rate (lb/MMBtu) x Heat In	put (MMBtu/hr, HHV)								
CO Emission Rate (lb/MMBtu)	0.01584	0.01579	0.01570	0.01607	0.01565	0.01511	0.01657	0.01657	0.01700
Heat Input (MMBtu/hr, HHV)	2209.2	2090.2	1974.7	1742.8	1661.7	1588.3	1388.2	1327.9	1294.4
CO Emission Rate (lb/hr)	35.0	33.0	31.0	28.0	26.0	24.0	23.0	22.0	22.0
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure (% VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfm)		12.5 lb/ft² (pres	ssure) / [1545.4 f	t-lh (age coneta	nt.R) x Actual :	Temp. (°R)] x 60	min/hr		
Basis, ppm actual Basis, ppmvd @ 15% O₂ - Moisture (%) Oxygen (%) wet Oxygen (%) dry Elow (acfm)	1.40 1.02 8.05 12.40 13.49 2.859.044	1,40 1,03 9,16 12,34 13,58 2,806,249	1.40 1.00 10.62 12.09 13.53 2.699.692	1.40 1.05 7.89 12.58 13.66	1.40 1.00 9.34 12.15 13.40	1.40 0.96 10.89 11.79 13.23 2.195.150	1.40 1.06 7 87 12.61 13.69	1.40 1.06 8.95 12.58 13.82 1 950 402	1.40 1.07 10.23 12.53 13.96
Basis, ppmvd @ 15% O₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm)	1.02 8.05 12.40 13.49 2,859,044	1.03 9.16 12.34 13.58 2,806,249	1.00 10.62 12.09 13.53 2,699,692	1.40 1.05 7.89 12.58 13.66 2,320,884	1.40 1.00 9.34 12.15 13.40 2,259,352	0.96 10.89 11.79 13.23 2,195,150	1.40 1.06 7.87 12.61 13.69 1,965,032	1.06 8.95 12.58 13.82 1.950,402	1.07 10.23 12.53 13.96 1,966,618
Basis, ppmvd @ 15% O₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry	1.02 8.05 12.40 13.49 2.859,044 2,628,891	1.03 9.16 12.34 13.58 2,806,249 2,549,197	1.00 10.62 12.09 13.53 2,699,692 2.412,985	1,40 1,05 7,89 12,58 13,66 2,320,884 2,137,766	1.40 1.00 9.34 12.15 13.40 2,259,352 2,048,329	0.96 10.89 11.79 13.23 2,195,150 1,956,098	1.40 1.06 7.87 12.61 13.69 1,965,032 1,810,384	1.06 8.95 12.58 13.82 1.950,402 1,775,841	1.07 10.23 12.53 13.96 1,966,618
Basis, ppmvd @ 15% O₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm) Flow (acfm) Elwhaust Temperature (°F)	1.02 8.05 12.40 13.49 2,859,044 2,628,891 1,098	1.03 9.16 12.34 13.58 2,806,249 2,549,197 1,117	1.00 10.62 12.09 13.53 2,699,692 2.412,985 1,132	1,40 1.05 7,89 12,58 13,66 2,320,884 2,137,766 1,109	1,40 1,00 9,34 12,15 13,40 2,259,352 2,048,329 1,174	0.96 10.89 11.79 13.23 2,195,150	1.40 1.06 7.87 12.61 13.69 1,965,032	1.06 8.95 12.58 13.82 1.950,402	1.07 10.23 12.53 13.96 1,966,615 1,765,43
Basis, ppmvd @ 15% O₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry	1.02 8.05 12.40 13.49 2.859,044 2,628,891	1.03 9.16 12.34 13.58 2,806,249 2,549,197	1.00 10.62 12.09 13.53 2,699,692 2.412,985	1,40 1,05 7,89 12,58 13,66 2,320,884 2,137,766	1.40 1.00 9.34 12.15 13.40 2,259,352 2,048,329	0.96 10.89 11.79 13.23 2,195,150 1,956,098 1,209	1.40 1.06 7.87 12.61 13.69 1,965,032 1,810,384 1,202	1.06 8.95 12.58 13.82 1.950,402 1,775,841 1,215	1.07 10.23 12.53 13.96 1,966,619 1,765,43 1,215
Basis, ppmvd @ 15% O₂ - Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) as methane	1.02 8.05 12.40 13.49 2.859,044 2.628,891 1,098 3.37	1.03 9.16 12.34 13.58 2,806,249 2,549,197 1,117 3.27	1.00 10.62 12.09 13.53 2,699,692 2.412,985 1,132 3.12	1.40 1.05 7.89 12.58 13.66 2,320,884 2,137,766 1,109 2.72	1.40 1.00 9.34 12.15 13.40 2.259,352 2,048,329 1,174 2.54	0.96 10.89 11.79 13.23 2,195,150 1,956,098 1,209 2.42	1.40 1.06 7 87 12.61 13.69 1,965,032 1,810,384 1,202 2.17	1.06 8.95 12.58 13.82 1.950,402 1,775,841 1,215 2.14	1.07 10.23 12.53 13.96 1,966,615 1,765,43 1,215 2.16
Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (*F) VOC Emission Rate (lb/hr) as methane Sulfuric Acid Mist (SAM)	1.02 8.05 12.40 13.49 2.859,044 2.628,891 1.098 3.37 NA	1.03 9.16 12.34 13.58 2.806,249 2,549,197 1,117 3.27 3.3	1.00 10.62 12.09 13.53 2,699,692 2.412,985 1,132 3.12	1.40 1.05 7.89 12.58 13.66 2,320,884 2,137,766 1,109 2.72	1.40 1.00 9.34 12.15 13.40 2.259,352 2,048,329 1,174 2.54	0.96 10.89 11.79 13.23 2,195,150 1,956,098 1,209 2.42	1.40 1.06 7 87 12.61 13.69 1,965,032 1,810,384 1,202 2.17	1.06 8.95 12.58 13.82 1.950,402 1,775,841 1,215 2.14	1.07 10.23 12.53 13.96 1,966,615 1,765,43 1,215 2.16
Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) as methane Sulfuric Acid Mist (SAM) Sulfuric Acid Mist (lb/hr)= SO ₂ Emission Rate (lb/hr)	1.02 8.05 12.40 13.49 2.859,044 2.628,891 1.098 3.37 NA	1.03 9.16 12.34 13.58 2.806,249 2,549,197 1.117 3.27 3.3 by weight)/100	1.00 10.62 12.09 13.53 2,699,692 2.412,985 1,132 3.12 NA	1.40 1.05 7.89 12.58 13.66 2.320.884 2,137.768 1,109 2.72 NA	1.40 1.00 9.34 12.15 13.40 2.259,352 2.048,329 1.174 2.54 NA	0.96 10.89 11.79 13.23 2,195,150 1,956,098 1,209 2.42 NA	1.40 1.06 7 87 12.61 13.69 1.965.032 1.810,384 1,202 2.17 NA	1.06 8.95 12.58 13.82 1.950,402 1,775,841 1,215 2.14 NA	1.07 10.23 12.53 13.96 1,966,615 1,765,43 1,215 2.16 NA
Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) as methane Sulfuric Acid Mist (SAM) Sulfuric Acid Mist (lb/hr)= SO ₂ Emission Rate (lb/hr) SO ₂ Emission Rate (lb/hr)	1.02 8.05 12.40 13.49 2.859,044 2.628,891 1,098 3.37 NA	1.03 9.16 12.34 13.58 2.806,249 2,549,197 1,117 3.27 3.3 by weight)/100 11.7	1.00 10.62 12.09 13.53 2.699,692 2.412,985 1,132 3.12 NA	1.40 1.05 7.89 12.58 13.66 2.320,884 2.137,766 1.109 2.72 NA	1.40 1.00 9.34 12.15 13.40 2.259,352 2.048,329 1.174 2.54 NA	0.96 10.89 11,79 13.23 2,195,150 1,956,098 1,209 2.42 NA	1.40 1.06 7.87 12.61 13.69 1.965.032 1.810.384 1,202 2.17 NA	1.06 8.95 12.58 13.82 1.950,402 1,775,841 1,215 2,14 NA	1.07 10.23 12.53 13.96 1,966,615 1,765,43 1,215 2.16 NA
Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) as methane Sulfuric Acid Mist (SAM) Sulfuric Acid Mist (lb/hr)= SO ₂ Emission Rate (lb/hr)	1.02 8.05 12.40 13.49 2.859,044 2.628,891 1.098 3.37 NA	1.03 9.16 12.34 13.58 2.806,249 2,549,197 1.117 3.27 3.3 by weight)/100	1.00 10.62 12.09 13.53 2,699,692 2.412,985 1,132 3.12 NA	1.40 1.05 7.89 12.58 13.66 2.320.884 2,137.768 1,109 2.72 NA	1.40 1.00 9.34 12.15 13.40 2.259,352 2.048,329 1.174 2.54 NA	0.96 10.89 11.79 13.23 2,195,150 1,956,098 1,209 2.42 NA	1.40 1.06 7 87 12.61 13.69 1.965.032 1.810,384 1,202 2.17 NA	1.06 8.95 12.58 13.82 1.950,402 1,775,841 1,215 2.14 NA	1.07 10.23 12.53 13.96 1,966,615 1,765,43 1,215 2.16 NA

Note: ppmvd= parts per million, volume dry; O₂= oxygen.







Table GE-A-3: Design Information and Stack Parameters - Simple Cycle Operation (GE 7FA.05) Dry Low NO_x Combustor, ULSD Oil, Base Load

					CT Only				
		l Turbine inlet Te		75% Load	Turbine Inlet Te	mperature	50% Load	Turbine Inlet Te	mperature
Parameter	35° F	75° F	95° F	35° F	75° F	95° F	35° F	75° F	95° F
Combustion Turbine Performance									
Heat Input (MMBtu/hr, LHV)	2,121.3	2,121.3	2.002.9	1.691.8	1.672.7	1,589,4	1,315.7	1,285.1	1.224.0
Heat Input (MMBtu/hr, HHV)	2,121.3	2,121.3	2,002.9	1.802.7	1,782.3	1,693.6	1,401.9	1,269.3	1,304.2
Evaporative Cooler	None	None	2,134.2 None	None	None	None	None	None	None
Relative Humidity (%)	60	60	60	60	60	60	60	60	60
Fuel heating value (Btu/lb, LHV)	18,300	18.300	18,300	18.300	18,300	18.300	18.300		18.300
Fuel heating value (Blu/lb, HHV)	19,499	19,499						18,300	
	1,066		19,499	19,499	19,499	19,499	19,499	19,499	19,499
Ratio of fuel heating values (HHV/LHV)	1.000	1.066	1.066	1.066	1.066	1.066	1.066	1.066	1.066
CT Exhaust Flow									
Volume flow (acfm) = [Mass flow (lb/hr) x 15	45.4 x Temp (°F	+ 460 K)] / [2112.:	5 x 60 min/hr x MV	(see note below	for constants)				
Mass Flow (lb/hr)	4,040,000	4,198,000	4,028,000	3,285,000	3,233,000	3,128,000	2,627,000	2.634,000	2,586,000
Temperature (°F)	1,107	1,106	1,118	1,143	1,177	1,190	1,215	1,215	1,215
Moisture (% Vol.)	11.71	12.50	13.29	10.99	12.17	12.92	10.24	10.99	11,65
Oxygen (% Vol.)	10.53	10.70	10.68	10.82	10.57	10.58	11.17	11.24	11,34
Molecular Weight	28.31	28.20	28.10	28.37	28.24	28.15	28.44	28.34	28.25
Volume flow (acfm)	2,726,718	2,842,493	2.758,200	2,262,907	2,284,721	2,235,368	1,886,229	1,897,966	1,869,632
Fuel Usage									
Fuel usage (lb/hr) = Heat Input (MMBtu/hr)	x 1 000 000 Btu/N	MRtu [Fuel Heat	Content Rtu/lb (Lt	1//)1					
Heat input (MMBtu/hr, LHV)	2.121.3	2.121.3	2.002.9	1,691.8	1,672.7	1.589.4	1,315.7	1,285.1	1.224.0
Heat content (Btu/lb, LHV)	18.300	18.300	18,300	18.300	18,300	18,300	18,300	18,300	18,300
Fuel usage (lb/hr)	115,918	115,918	109.448	92,448	91,404	86,852	71,896	70,224	66.885
Fuel usage (ID/III)	113,510	115,516	109,440	92.446	91,404	60,652	71,050	70,224	00,003
CT Stack Parameters									
Stack Height (feet)	80	80	80	80	80	80	80	80	80
Stack Diameter (feet)	23	23	23	23	23	23	23	23	23
CT Stack Flow Conditions									
Velocity (ft/sec) = Volume flow (acfm) / [((di	ameter)² /4) x 3.1-	4159] / 60 sec/mir	า						
Stack Temperature (°F)	1,107	1,106	1,118	1,143	1,177	1,190	1,215	1,215	1,215
Volume flow (acfm)	2,726,718	2,842,493	2,758,200	2,262,907	2,284,721	2,235,368	1,886,229	1,897,966	1,869,632
Diameter (feet)	23	23	23	23	23	23	23	23	23
	109.4	114.0	110.6	90.8	91.7	89.7	75.7	76.1	75.0

Note: Universal gas constant = 1,545.4 ft-lb(force)/*R; atmospheric pressure = 2,112.5 lb(force)/ft² (@14.67 psia).





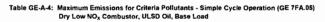


Table GE-A-4: Maximum Emissions for Criteria Pollutants - Simple Cycle Operation (GE 7FA.05)
Dry Low NO₃ Combustor, ULSD Oil, Base Load

					CT Only				
		ad Turbine Inlet Ten			d Turbine Inlet Tem			d Turbine Inlet Tem	
Parameter	35° F	75° F	95° F	35° F	75° F	95° F	35° F	75° F	95° F
Particulate Matter (PM10/PM2.5)									
PM 10/PM 25 (lb/hr) = PM 10 Emissions Rate (lb/MME	Stu) x Heat Input (MMBtu/hr, F	HV) (front-half & bac	k-half)						
PM ₁₀ Emission Rate (lb/MMBtu, HHV)	0.01641	0.01641	0.01738	0.02058	0.02082	0.02191	0.02646	0.02709	0.02845
Heat Input (MMBtu/hr, HHV)	2,260.3	2,260.3	2,134.2	1,802.7	1,782.3	1,693.6	1,401,9	1,369.3	1,304,2
PM ₁₀ /PM _{2.5} Emission Rate (lb/hr)	37.1	37.1	37 1	37.1	37.1	37.1	37.1	37.1	37.1
	NA	37.1	NA	NA	NA	NA	NA	NA	NA
Sulfur Dioxide (SO ₂)									
SO 2 (lb/hr)= Fuel oil (lb/hr) x sulfur content(% weigh	t) x (lb SO 2 /lb S) /100								
Fuel oil Sulfur Content	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%
Fuel oil use (lb/hr)	115,918	115,916	109,448	92,448	91,404	86,852	71,896	70,224	86,885
Ib SO ₂ / Ib S (64/32)	2	2	2	2	2	2	2	2	2
SO ₂ Emission Rate (lb/hr)	3.48	3.5	3.3	2.77	2.7	2.6	2.18	2.1	2.0
SO 2 (lb/hr) = SO 2 Emissions Rate (lb/MMBtu) x He	at Input (MMBtu/hr, HHV)								
SO ₂ Emission Rate (lb/MMBtu) (HHV)	0.001803	0.001603	0.001603	0.001803	0.001603	0.001603	0.001603	0.001603	0.001803
Heat Input (MMBtu/hr, HHV)	2,260.3	2,260.3	2,134.2	1,802,7	1,782.3	1,693,6	1,401.9	1,369.3	1,304.2
SO ₂ Emission Rate (lb/hr)	3.62	3.82	3.42	2.89	2.86	2.72	2.25	2.20	2.09
No, (ppmv actual) = NO, (ppmd @ 15%O ₂) x [(20	0 0 des//20 0 1531 × [1	Mainture (94 \/100)							
Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (Moisture (36)/ 100j							
NO , (lb/hr) = NO , (ppm actual) x Volume flow (acfm	n) x 46 (mole. wgt NO ,) x 21	12.5 lb/ft² (pressure)	/[1545.4 ft-lb (gas cons	tant, R) x Actual Temp	. (°R)] x 60 min/hr				
Basis, ppm actual	56.4	54.0	53.0	55.4	55.4	54.2	54.0	52.4	50.7
NO _x , ppmvd @15% O ₂	42.0	42.0	42.0	42.0	42.0	42.0	42.0	42.0	42.0
Moisture (%)	11.71	12.50	13.29	10.99	12.17	12.92	10.24	10.99	11.85
Oxygen (%)	10.53	10.70	10.68	10.82	10.57	10.58	11.17	11.24	11,34
Oxygen (%) dry	11.93	12.23	12.32	12.18	12.03	12.15	12.44	12.63	12.84
Flow (acfm)	2,726,718	2,842,493	2,758,200	2,262,907	2,284,721	2,235,368	1,886,229	1,897,968	1,869,632
Flow (acfm), dry	2,407,419	2,487,181	2,391,635	2,014,213	2,006,671	1,946,559	1,693,079	1,689,380	1,651,820
Exhaust Temperature (°F)	1,107	1,106	1,118	1,143	1,177	1,190	1,215	1,215	1,215
	370.3	369.9	349.4	295.1	291,9	277.2	229.5	224.1	213.6
NO _x Emission Rate (lb/hr)		369.0	349.0	294.0	291.0	277.0	229.0	224.0	213.0
NO _x Emission Rate (lb/hr)	369.0								
NO , (lb/hr) = NO , Emissions Rate (lb/MMBlu) x He	eat Input (MMBtu/hr, HHV)								
NO, (llb/hr) = NO, Emissions Rate (llb/MMBtu) x He NO, Emission Rate (llb/MMBtu)	eat Input (MMBtu/hr, HHV) 0.16325	0.16325	0.16353	0.16309	0.16327	0.16356	0,18335	0.16358	0.16332
NO, (lb/hr) = NO, Emissions Rate (lb/MMBlu) x He	eat Input (MMBtu/hr, HHV)	0.16325 2260.3 369.0	0.16353 2134.2	0.16309 1802.7	0.16327 1782.3	0.16356 1693.6	0,18335 1401.9	0.16358 1369.3	0.16332 1304.2 213.0







					CT Only				
		ad Turbine Inlet Ten			d Turbine Inlet Tem			d Turbine Inlet Tem	
Parameter	35° F	75° F	95° F	35° F	75° F	95° F	35° F	75° F	95° F
Carbon Monoxide (CO)									
CO (ppmv wet or actual) = CO (ppmvd @ 15%O 2):	x [(20.9 - O 2 dry)/(20.9 - 15)] x	(1- Moisture(%)/100)	1						
Oxygen (%, dry)(O 2 dry) = Oxygen (%)/[1-Moisure	(%)]								
CO (lb/hr) = CO (ppm actual) x Volume flow (acfm)	x 28 (male, wat CO) x 2112 5 I	h/ft ² (pressure) / [15	45 4 ft-lh (oas constant	R) x Actual Temp CR)t v 60 minAr				
Basis, ppm actual	17.66	17.50	17.34	17.80	17.57	17.42	17.95	17.80	17.67
Basis, ppmvd	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0
Basis, ppmvd @ 15% O ₂	13.15	13.61	13.75	13.49	13.31	13.49	13.96	14.26	14.63
Moisture (%)	11.71	12.50	13.29	10.99	12.17				
Oxygen (%)	10.53	10.70	10.68	10.99	12.17	12.92 10.58	10.24	10.99	11.65
Oxygen (%) dry	11.93	12.23	12.32	12.16	12.03	10.58	11.17 12.44	11.24	11.34 12.84
Flow (acfm)	2,726,718	2,842,493	2,758,200	2,262,907	2,284,721	2,235,368	1,886,229	12.63 1.897,966	1,869,632
Flow (acfm), dry	2,407,419	2,487,181	2,730,200	2,262,807	2,204,721	1,948,559	1,693,079	1,689,380	1,651,820
Exhaust Temperature (°F)	1.107	1,106	1,118	1,143	1,177	1,190	1,093,079	1,089,300	1,031,020
CO Emission Rate (lb/hr)	70.6	72.9	69.6	57.7	56.3	54.2	46.4	46.3	45.3
CO Emission read (Iprill)	71.0	73.0	70.0	58.0	56.0	54.2 54.0	46.4 46.0	46.3 46.0	45.3 45.0
	71.0	70.0	70.0	30,0	30.0	34.0	40.0	40.0	43.0
CO (lb/hr) = CO Emissions Rate (lb/MMBtu) x Heat	Input (MMBtu/hr. HHV)								
CO Emission Rate (lb/MMBtu)	0.03141	0.03230	0.03280	0.03217	0.03142	0.03189	0.03281	0.03359	0.03450
Heat Input (MMBtu/hr, HHV)	2,260.3	2,280.3	2,134.2	1.802.7	1,782.3	1,693.6	1,401.9	1,369.3	1,304.2
CO Emission Rate (lb/hr)	71.0	73.0	70.0	58.0	56.0	54.0	46.0	46.0	45.0
(olatile Organic Compounds (VOC) (OC (ppmv wet or actual) = VOC (ppmvd @ 15%O (Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure	(%)]		•						
/olatile Organic Compounds (VOC) /OC (ppmv wet or actual) = VOC (ppmvd @ 15%O oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure /OC (lb/hr) = VOC (ppm actual) x Volume flow (acfi	(%)] m) x 16 (mole. wgt CH ₄) x 211	2.5 lb/ft ² (pressure)	/ [1545.4 ft-lb (gas cons						
folatile Organic Compounds (VOC) /OC (ppmv wet or actual) = VOC (ppmvd @ 15%O xxygen (%, dry)(O ₂ dry) = Oxygen (%)/f1-Moisure /OC (lb/hr) = VOC (ppm actual) x Volume flow (ach Basis, ppm actual)	(%)] m) x 16 (mole. wgt CH ₄) x 211 3.50	2.5 lb/ft ² (pressure) a 3.50	/ [1545.4 ft-lb (gas cons 3.50	5.19	5.26	5.19	5.02	4.91	4.78
folatile Organic Compounds (VOC) //OC (ppmv wet or actual) = VOC (ppmvd @ 15%O Daygen (%, dry)(O, dry) = Oxygen (%)/11-Moisure //OC (lb/tr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual) Basis, ppmvd @ 15% O ₂	(%)] m) x 16 (mole. wgt CH 4) x 211 3.50 2.03	2.5 lb/ft ² (pressure) a 3.50 2.08	/ [1545.4 ft-lb (gas cons 3.50 2.09	5.19 3.93	5.26 3.98	4.02	3.90	3.93	3.96
Colatile Organic Compounds (VOC)	(%)] m) x 16 (mole. wgt CH ₄) x 211 3.50 2.03 11.71	2.5 lb/ft ² (pressure) / 3.50 2.08 12.50	/ [1545.4 ft-lb (gas cons 3.50 2.09 13.29	5.19 3.93 10.99	5.26 3.98 12.17	4.02 12.92	3.90 10.24	3.93 10.99	3.96 11.65
folatile Organic Compounds (VOC) /OC (ppmv wet or actual) = VOC (ppmvd @ 15%O /OXygen (%, dry)(O ₂ dry) = Oxygen (%)/1-Moisure /OC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Cxygen (%) wet	(%)] m) x 16 (mole. wgt CH ₄) x 211 3.50 2.03 11.71 10.53	2.5 lb/ft ² (pressure) 3.50 2.08 12.50 10.70	/[1545.4 ft-lb (gas cons 3.50 2.09 13.29 10.88	5.19 3.93 10.99 10.82	5.26 3.98 12.17 10.57	4.02 12.92 10.58	3.90 10.24 11.17	3.93 10.99 11.24	3.96 11.65 11.34
tolatile Organic Compounds (VOC) (OC (ppmv wet or actual) = VOC (ppmvd @ 15%O (Oxygen (%, dry)(O, dry) = Oxygen (%)/[1-Moisure (OC (lb/hr) = VOC (ppm actual) x Volume flow (actilibasis, ppm actual) Basis, ppmd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry	(%)] m) x 16 (mole. wgt CH ₄) x 211 2.03 11.71 10.53 11.93	2.5 lb/ft ² (pressure) / 3.50 2.08 12.50 10.70 12.23	/[1545.4 ft-lb (gas cons 3.50 2.09 13.29 10.88 12.32	5.19 3.93 10.99 10.82 12.16	5.26 3.98 12.17 10.57 12.03	4.02 12.92 10.58 12.15	3.90 10.24 11.17 12.44	3.93 10.99 11.24 12.63	3.96 11.65 11.34 12.84
folatile Organic Compounds (VOC) //OC (ppmv wet or actual) = VOC (ppmvd @ 15%O //OC (lb/mr) = VOC (ppm actual) = VOG (m/mr) = VOC (ppm actual) x Volume flow (acfi //OC (lb/mr	(%)] m) x 16 (mole. wgt CH ₊) x 211 3.50 2.03 11.71 10.53 11.93 2.726,718	2.5 lb/ft ² (pressure) / 3.50 2.08 12.50 10.70 12.23 2.842,493	/ [1545.4 ft-lb (gas cons 3.50 2.09 13.29 10.88 12.32 2,758,200	5.19 3.93 10.99 10.82 12.16 2,262,907	5.26 3.98 12.17 10.57 12.03 2,284,721	4.02 12.92 10.58 12.15 2,235,368	3.90 10.24 11.17 12.44 1,886,229	3.93 10.99 11.24 12.63 1,897,966	3.96 11.65 11.34 12.84 1,869,632
folatile Organic Compounds (VOC) //OC (ppmv wet or actual) = VOC (ppmvd @ 15%O Dxygen (%, dry)(O ₂ dry) = Oxygen (%)/11-Moisure //OC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry	(%)] m) x 16 (mole. wgt CH ₊) x 211 3.50 2.03 11.71 10.53 11.93 2.726,718 2.407,419	2.5 lb/ft ² (pressure) . 3.50 2.08 12.50 10.70 12.23 2.842,493 2.467,181	/ [1545.4 ft-lb (gas cons 3.50 2.09 13.29 10.88 12.32 2.758,200 2.391,635	5.19 3.93 10.99 10.82 12.16 2,262,907 2,014,213	5.26 3.98 12.17 10.57 12.03 2.284.721 2,006.671	4.02 12.92 10.58 12.15 2,235,368 1,946,559	3.90 10.24 11.17 12.44 1,886,229 1,693,079	3.93 10.99 11.24 12.63 1,897,966 1,669,360	3.96 11.65 11.34 12.84 1,869,632 1,651,820
tolatile Organic Compounds (VOC) OC (ppmv wet or actual) = VOC (ppmvd @ 15%O xxygen (%, dry)(O ₂ dry) = Oxygen (%)/1-Moisure OC (lb/hr) = VOC (ppm actual) x Volume flow (ach Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (achm)	(%)] m) x 16 (mole. wgt CH ₊) x 211 3.50 2.03 11.71 10.53 11.93 2.726,718 2.407,419 1,107	2.5 lb/ft ² (pressure) , 3.50 2.08 12.50 10.70 12.23 2.842,493 2.467,181 1,106	/ [1545.4 ft-lb (gas cons 3.50 2.09 13.29 10.88 12.32 2.758.200 2.391.635 1,118	5.19 3.93 10.99 10.82 12.16 2,262,907 2,014,213 1,143	5.26 3.98 12.17 10.57 12.03 2.284,721 2,006,671 1,177	4.02 12.92 10.58 12.15 2,235.368 1,946,559 1,190	3.90 10.24 11.17 12.44 1,886,229 1,693,079 1,215	3.93 10.99 11.24 12.63 1.897,966 1,669,380 1,215	3.96 11.65 11.34 12.84 1,869,632 1,651,820 1,215
folatile Organic Compounds (VOC) /OC (ppmv wet or actual) = VOC (ppmvd @ 15%O /OXygen (%, dry)(O ₂ dry) = Oxygen (%)/f1-Moisure /OC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm)	(%)] m) x 16 (mole. wgt CH ₊) x 211 3.50 2.03 11.71 10.53 11.93 2.726,718 2.407,419	2.5 lb/ft ² (pressure) . 3.50 2.08 12.50 10.70 12.23 2.842,493 2.467,181	/ [1545.4 ft-lb (gas cons 3.50 2.09 13.29 10.88 12.32 2.758,200 2.391,635	5.19 3.93 10.99 10.82 12.16 2,262,907 2,014,213	5.26 3.98 12.17 10.57 12.03 2.284.721 2,006.671	4.02 12.92 10.58 12.15 2,235,368 1,946,559	3.90 10.24 11.17 12.44 1,886,229 1,693,079	3.93 10.99 11.24 12.63 1,897,966 1,669,360	3.96 11.65 11.34 12.84 1,869,632 1,651,820
Volatile Organic Compounds (VOC) VOC (ppmv wet or actual) = VOC (ppmvd @ 15%O Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/1-Moisure VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) oty Flow (acfim)	(%)] m) x 16 (mole. wgt CH ₊) x 211 3.50 2.03 11.71 10.53 11.93 2.726,718 2.407,419 1.107 7.99	2.5 lb/ft ² (pressure) . 3.50 2.08 12.50 10.70 12.23 2.842,493 2.487,181 1,106 8.34	/ [1545.4 ft-lb (gas cons 3.50 2.09 13.29 10.88 12.32 2.758.200 2.391.635 1,118 8.03	5.19 3.93 10.99 10.82 12.16 2,262,907 2,014,213 1,143 9.81	5.26 3.98 12.17 10.57 12.03 2.284,721 2,006,671 1,177 9.63	4.02 12.92 10.58 12.15 2,235,368 1,946,559 1,190 9,23	3.90 10.24 11.17 12.44 1,886,229 1,693,079 1,215 7,41	3.93 10.99 11.24 12.63 1.897,966 1.669,360 1.215 7.30	3.96 11.65 11.34 12.84 1,869,632 1,651,820 1,215 7.01
Volatile Organic Compounds (VOC) VOC (ppmv wet or actual) = VOC (ppmvd @ 15%O Dxygen (%, dry)(O ₂ dry) = Oxygen (%)/1-Moisure VOC (lb/rr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm), dry Exhaust Temperature (*F) VOC Emission Rate (lb/hr)	(%)] m) x 16 (mole. wgt CH ₊) x 211 3.50 2.03 11.71 10.53 11.93 2.726,718 2.407,419 1.107 7.99 NA	2.5 lb/lt ² (pressure) . 3.50 2.08 12.50 10.70 12.23 2.842,493 2.467,181 1.106 8.34 6.20	/ [1545.4 ft-lb (gas cons 3.50 2.09 13.29 10.88 12.32 2.758.200 2.391.635 1,118 8.03	5.19 3.93 10.99 10.82 12.16 2,262,907 2,014,213 1,143 9.81	5.26 3.98 12.17 10.57 12.03 2.284,721 2,006,671 1,177 9.63	4.02 12.92 10.58 12.15 2,235,368 1,946,559 1,190 9,23	3.90 10.24 11.17 12.44 1,886,229 1,693,079 1,215 7,41	3.93 10.99 11.24 12.63 1.897,966 1.669,360 1.215 7.30	3.96 11.65 11.34 12.84 1,869,632 1,651,820 1,215 7.01
Colatile Organic Compounds (VOC) VOC (ppmv wet or actual) = VOC (ppmvd @ 15%O Nxygen (%, dry)(O, dry) = Oxygen (%)/f1-Moisure (VOC (lb/hr) = VOC (ppm actual) x Volume flow (actile Basis, ppmvd @ 15% O, Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (actm) dry Flow (actm) dry Exhaust Temperature ("F) VOC Emission Rate (lb/hr) Sulfuric Acid Mist (lb/hr) = SO, Emission Rate (lb/hr) Sulfuric Acid Mist (lb/hr) = SO, Emission Rate (lb/hr)	(%)] m) x 16 (mole. wgt CH ₊) x 211 3.50 2.03 11.71 10.53 11.93 2.726,718 2.407,419 1.107 7.99 NA	2.5 lb/lt ² (pressure) . 3.50 2.08 12.50 10.70 12.23 2.842,493 2.467,181 1.106 8.34 6.20	/ [1545.4 ft-lb (gas cons 3.50 2.09 13.29 10.88 12.32 2.758.200 2.391.635 1,118 8.03	5.19 3.93 10.99 10.82 12.16 2,262,907 2,014,213 1,143 9.81	5.26 3.98 12.17 10.57 12.03 2.284,721 2,006,671 1,177 9.63	4.02 12.92 10.58 12.15 2,235,368 1,946,559 1,190 9,23	3.90 10.24 11.17 12.44 1,886,229 1,693,079 1,215 7,41	3.93 10.99 11.24 12.63 1.897,966 1.669,360 1.215 7.30	3.96 11.65 11.34 12.84 1,869,632 1,651,820 1,215 7.01
Totatile Organic Compounds (VOC) OC (ppmv wet or actual) = VOC (ppmvd @ 15%O Dxygen (%, dry)/O 2 dry) = Oxygen (%)/1-Moisure OC (lb/hr) = VOC (ppm actual) x Volume flow (ach Basis, ppmvd @ 15% O 2 Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm) Flow (acfm) Flow (acfm) Acfm) Acfm) Acfm (b/hr) So 2 Emission Rate (lb/hr) SO 2 Emission Rate (lb/hr)	(%)] m) x 16 (mole. wgt CH ₊) x 211 3.50 2.03 11.71 10.53 11.93 2.726,718 2.407,419 1.107 7.99 NA	2.5 lb/lt ² (pressure) . 3.50 2.08 12.50 10.70 12.23 2.467,181 1.106 8.34 6.20 by weight//100	/ [1545.4 fi-lb (gas cons 3.50 2.09 13.29 10.88 12.32 2,758,200 2.391,635 1,118 8.03 NA	5.19 3.93 10.99 10.82 12.16 2.282,907 2.014,213 1,143 9.81 NA	5.28 3.98 12.17 10.57 12.03 2.284,721 2.008.671 1.177 9.63 NA	4.02 12.92 10.58 12.15 2.235.388 1.946.559 1.190 9.23 NA	3.90 10.24 11.17 12.44 1.886.229 1.683,079 1.215 7.41 NA	3.93 10.99 11.24 12.63 1.897,986 1.669,380 1.215 7.30 NA	3.96 11.85 11.34 12.84 1,869,832 1,651,820 1,215 7.01 NA
Volatile Organic Compounds (VOC) VOC (ppmv wet or actual) = VOC (ppmvd @ 15%O Dxygen (%, dry)(O ₂ dry) = Oxygen (%)/1-Moisure VOC (lb/rr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm), dry Exhaust Temperature (*F) VOC Emission Rate (lb/hr)	(%)] m) x 16 (mole. wgt CH ₊) x 211 3.50 2.03 11.71 10.53 11.93 2.726,718 2.407,419 1.107 7.99 NA	2.5 lb/lt ² (pressure) . 3.50 2.08 12.50 10.70 12.23 2.842,493 2.487,181 1,106 8.34 6.20 by weight)/100 3.6	/ [1545.4 fi-lb (gas cons 3.50 2.09 13.29 10.88 12.32 2.758,200 2.391,635 1.116 8.03 NA	5.19 3.93 10.99 10.82 12.16 2.262.907 2.014.213 1.143 9.81 NA	5.26 3.98 12.17 10.57 12.03 2.284,721 2.006,871 1,177 9.63 NA	4.02 12.92 10.55 12.15 2.255,368 1,946,559 1,190 9.23 NA	3.90 10.24 11.17 12.44 1.866.229 1,693.079 1,215 7.41 NA	3.93 10.99 11.24 12.63 1.897,966 1.669,380 1,215 7.30 NA	3.96 11.65 11.34 12.84 1.869,632 1.651,820 1.215 7.01 NA
Volatile Organic Compounds (VOC) VOC (ppmv wet or actual) = VOC (ppmvd @ 15%O Oxygen (%, dry)(O, dry) = Oxygen (%)/1-Molsure VOC (lb/hr) = VOC (ppm actual) x Volume flow (acti Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (actim) Flow (actim) Flow (actim) Flow (actim) VOC Emission Rate (lb/hr) Sulfluric Acid Mist (lb/hr) = SO ₂ Emission Rate (lb/hr) Sulfluric Acid Mist (lb/hr) = SO ₂ Emission Rate (lb/hr) Conversion to H ₂ SO ₄ (% by weight)	(%)] m) x 16 (mole. wgt CH ₊) x 211 3.50 2.03 11.71 10.53 11.93 2.726,718 2.407,419 1.107 7.99 NA	2.5 lb/lt ² (pressure) . 3,50 2,08 12,50 10,70 12,23 2,842,493 2,467,181 1,106 8,34 6,20 by weight//100 3,6 10	/ [1545.4 ft-lb (gas cons 3.50 2.09 13.29 10.88 12.32 2.758.200 2.391.635 1,116 8.03 NA	5.19 3.93 10.99 10.82 12.16 2.262,907 2.014,213 1,143 9.81 NA	5.28 3.98 12.17 10.57 12.03 2.284,721 2.006,871 1,177 9.63 NA	4.02 12.92 10.59 12.15 12.15, 368 1.946,559 1.190 9.23 NA	3.90 10.24 11.17 12.44 1.886.229 1.683.079 1.215 7.41 NA	3.93 10.99 11.24 12.63 1.897,966 1,869,360 1,215 7.30 NA	3.96 11.65 11.34 12.84 1.869,632 1,651,820 1,215 7.01 NA
folatile Organic Compounds (VOC) //OC (ppmv wet or actual) = VOC (ppmvd @ 15%O //OC (ppmv wet or actual) = VOC (ppmvd @ 15%O //OC (lb/hr) = VOC (ppm actual) x Volume flow (acti //OC (lb/hr) = VOC (ppm actual) x Volume flow (acti //OC (lb/hr) = VOC (ppm actual) x Volume flow (acti //OC (lb/hr) = VOC (ppm actual) x Volume flow (acti //OC (lb/hr) = VOC (ppm actual) x Volume flow (acti //OC (%) wet //OC (%) weight	(%)] m) x 16 (mole. wgt CH ₊) x 211 3.50 2.03 11.71 10.53 11.93 2.726,718 2.407,419 1.107 7.99 NA c) x Conversion to H ₂ SO ₊ (% the second	2.5 lb/lt ² (pressure) . 3.50 2.08 12.50 10.70 12.23 2.842,493 2.467,181 1.106 8.34 6.20 by weight)/100 3.6 10 0.36	/ [1545.4 ft-lb (gas cons 3.50 2.09 13.29 10.88 12.32 2.758.200 2.391.635 1,116 8.03 NA	5.19 3.93 10.99 10.82 12.16 2.262,907 2.014,213 1,143 9.81 NA	5.28 3.98 12.17 10.57 12.03 2.284,721 2.006,871 1,177 9.63 NA	4.02 12.92 10.59 12.15 12.15, 368 1.946,559 1.190 9.23 NA	3.90 10.24 11.17 12.44 1.886.229 1.683.079 1.215 7.41 NA	3.93 10.99 11.24 12.63 1.897,966 1,869,360 1,215 7.30 NA	3.96 11.65 11.34 12.84 1.869,632 1,651,820 1,215 7.01 NA
/olatile Organic Compounds (VOC) //OC (ppmv wet or actual) = VOC (ppmvd @ 15%O //OC (ppmv wet or actual) = VOC (ppmvd @ 15%O //OC (lib/hr) = VOC (ppm actual) x Volume flow (acfi //OC (lib/hr) = VOC (ppm actual) //OC (lib/hr) = VOC	(%)] m) x 16 (mole. wgt CH ₊) x 211 3.50 2.03 11.71 10.53 11.93 2.726,718 2.407,419 1.107 7.99 NA c) x Conversion to H ₂ SO ₊ (% the second	2.5 lb/lt ² (pressure) . 3.50 2.08 12.50 10.70 12.23 2.842,493 2.467,181 1.106 8.34 6.20 by weight)/100 3.6 10 0.36	/ [1545.4 ft-lb (gas cons 3.50 2.09 13.29 10.88 12.32 2.758.200 2.391.635 1,116 8.03 NA	5.19 3.93 10.99 10.82 12.16 2.262,907 2.014,213 1,143 9.81 NA	5.26 3.98 12.17 10.57 12.03 2.284,721 2.006,671 1.177 9.63 NA	4.02 12.92 10.59 12.15 12.15, 368 1.946,559 1.190 9.23 NA	3.90 10.24 11.17 12.44 1.886.229 1.683.079 1.215 7.41 NA	3.93 10.99 11.24 12.63 1.897,966 1,869,360 1,215 7.30 NA	3.96 11.65 11.34 12.84 1.869,632 1,651,820 1,215 7.01 NA
### ### ##############################	(%)] m) x 16 (mole. wgt CH ₊) x 211 3.50 2.03 11.71 10.53 11.93 2.726,718 2.407,419 1.107 7.99 NA r) x Conversion to H ₂ SO ₄ (% l 3.6 10 0.36	2.5 lb/lt ² (pressure) . 3.50 2.08 12.50 10.70 12.23 2.842,493 2.487,181 1.106 8.34 6.20 by weight)/100 3.6 10 0.36	/ [1545.4 fi-lb (gas cons 3.50 2.09 13.29 10.88 12.32 2,756,200 2.391,635 1.118 8.03 NA	5.19 3.93 10.99 10.82 12.16 2.262.907 2.014.213 1.143 9.81 NA	5.28 3.98 12.17 10.57 12.03 2.284,721 2.006,871 1,177 9.63 NA	4.02 12.92 10.55 12.15 2.255.388 1.946,559 1.190 9.23 NA	3.90 10.24 11.17 12.44 1.866.229 1.693.079 1.215 7.41 NA	3.93 10.99 11.24 12.63 1.897,966 1.669,360 1.215 7.30 NA	3.96 11.65 11.34 12.84 18.89,632 1,651,820 1,215 7,01 NA

Note: ppmvd= parts per million, volume dry; O2= oxygen.



July 2013

Table GE-A-5: Regulated and Hazardous Air Pollutant Emission Factors and Emissions for the Combustion Turbine Firing Gas and Distillate Fuel Oil (GE 7FA.05

		Combusti	:		Combusti	ion Turbin	e		(TPY) h	(TPY) "		
		Natura				D Oil ^a		Scenario 1	Scenario 2	Maximum		
Pollutant	Reference	Emission Factor (lb/MMBtu)	Units	Emission Rate (lb/hr)	Reference	Emission Factor (lb/MMBtu)	Units	Emission Rate (lb/hr)	CT NG	CT NG & FO	1 CT	5 CT
1,3-Butadiene	b,c	4.30E-07	lb/MMBtu	8.99E-04	f,c	1.60E-05	lb/MMBtu	3.62E-02	1,52E-03	1.03E-02	1.03E-02	5.17E-0
Acetaldehyde	b	4.00E-05	lb/MMBtu	8.36E-02				0.00E+00	1.42E-01	1,21E-01	1.42E-01	7.09E-0
Acrolein	b	6.40E-06	lb/MMBtu	1.34E-02				0.00E+00	2.27E-02	1.93E-02	2.27E-02	1.13E-0
Benzene	b	1.20E-05	lb/MMBtu	2.51E-02	f	5.50E-05	lb/MMBtu	1.24E-01	4.25E-02	6.73E-02	6.73E-02	3.37E-0
	b	3.20E-05	lb/MMBtu	6.69E-02		3.30L-03		0.00E+00	1.13E-01	9.67E-02	1.13E-01	5.67E-0
Ethylbenzene	d				d							
Formaldehyde	b	2.03E-04	lb/MMBtu	4.23E-01	f	2.17E-04	ib/MMBtu	4.91E-01	7.18E-01	7.35E-01	7.35E-01	3.67E+0
Naphthalene Polycyclic Aromatic	b,e	1.30E-06	lb/MMBtu	2.72E-03	f,e	3.50E-05	lb/MMBtu	7.91E-02	4.61E-03	2.37E-02	2.37E-02	1.19E-0
Hydrocarbons (PAH)		2.20E-06	lb/MMBtu	4.60E-03	.,0	4.00E-05	fb/MMBtu	9.04E-02	7.79E-03	2.92E-02	2.92E-02	1.46E-0
Propylene Oxide	b,c	2.90E-05	lb/MMBtu	6.06E-02				0.00E+00	1.03E-01	8.76E-02	1.03E-01	5.14E-0
Toluene	b	3.30E-05	lb/MMBtu	6.90E-02				0.00E+00	1.17E-01	9.97E-02	1.17E-01	5.85E-0
Xylene	b	6.40E-05	lb/MMBtu	1.34E-01				0.00E+00	2.27E-01	1.93E-01	2.27E-01	1.13E+0
2-Methylnaphthalene				0.00E+00		-		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
3-Methylchloranthrene			-	0.00E+00			-	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
7,12-Dimethylbenz(a)anthracene			_	0.00E+00			-	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
Acenaphthene			-	0.00E+00				0.00E+00 0.00E+00	0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+0 0.00E+0
Acenaphthylene Anthracene			_	0.00E+00 0.00E+00			_	0.00E+00	0.00E+00 0.00E+00	0.00E+00	0.00E+00	0.00E+0
Benz(a)anthracene			-	0.00E+00			_	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
Benzo(a)pyrene			_	0.00E+00			_	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
Benzo(b)fluoranthene				0.00E+00			_	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
Benzo(g,h,i)perylene			-	0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
Benzo(k)fluoranthene			_	0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
Chrysene			-	0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
Dibenzo(a,h)anthracene				0.00E+00			-	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
Dichlorobenzene			-	0.00E+00			-	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
Fluoranthene				0.00E+00			-	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
Fluorene				0.00E+00				0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+0 0.00E+0
Hexane Indeno(1,2,3-cd)pyrene			-	0.00E+00 0.00E+00			-	0.00E+00 0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
Phenanathrene			-	0.00E+00			_	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
Pyrene			_	0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0
Arsenic				0.00E+00	g,c	1.10E-05	lb/MMBtu	2.49E-02	0.00E+00	6.22E-03	6.22E-03	3.11E-0
Beryllium			-	0.00E+00	g,c	3.10E-07	Ib/MMBtu	7.01E-04	0.00E+00	1.75E-04	1.75E-04	8.76E-0
Cadmium				0.00E+00 0.00E+00	g	4.80E-06	Ib/MMBtu	1.08E-02	0.00E+00	2.71E-03	2.71E-03	1.36E-0
			-		g					6.22E-03	6.22E-03	3.11E-0
Chromium Cobalt		 	-	0.00E+00 0.00E+00	ŭ	1.10E-05 	Ib/MMBtu	2.49E-02 0.00E+00	0.00E+00 0.00E+00	6.22E-03 0.00E+00	0.00E+00	0.00E+0
		-			g					7.91E-03	7.91E-03	3.96E-0
Lead			-	0.00E+00	9	1.40E-05	lb/MMBtu	3.16E-02	0.00E+00			
Manganese				0.00E+00	g	7.90E-04	lb/MMBtu	1.79E+00	0.00E+00	4.46E-01	4.46E-01	2.23E+0
Mercury			-	0.00E+00		1.20E-06	lb/MMBtu	2.71E-03	0.00E+00	6.78E-04	6.78E-04	3.39E-0
Nickel			-	0.00E+00	g,c	4.60E-06	lb/MMBtu	1.04E-02	0.00E+00	2.60E-03	2.60E-03	1.30E-0
Selenium				0.00E+00	g,c	2.50E-05	lb/MMBtu	5.65E-02	0.00E+00	1.41E-02	1.41E-02	7.06E-0
			Total HAPs =	0.88 0.42					1.50 0.72	1.48 0.73	1.59 0.73	7.95 3.67

a Emissions based on:

Fuel Natural gas Fuel oil
Heat input (MMBtu/hr) (HHV) (Baseload at 75 °F) 2,090 2,260

Building to the property of the propert

 Fuel
 Scenario 1
 Scenario 2

 Natural Gas
 3,390
 2,890

 Fuel Oil
 0
 500

 Total Hours
 3,390
 3,390

^c Based on the method detection limit; for the CT, based on 1/2 of the method detection limit; expected emissions are lower.

^d Formaldehyde emission factor based on 91 ppb @15% O₂ equivalent to combustion turbine MACT limit (see Table GE-A-6)

^e Assumed to be representative of Polycyclic Organic Matter (POM) emissions, a regulated HAP.

f Emission factor from Table 3.1-4, AP-42, EPA, April 2000.

⁹ Emission factor from Table 3.1-5, AP-42, EPA, April 2000.

h Annual operating hours

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Table GE-A-6: Maximum Formaldehyde Emissions When Firing Natural Gas and ULSD Oil (GE 7FA.05)

			CT at B	aseload		
	N	atural Gas-Firi	ng		ULSD Oil-Firing	g
	Turbi	ne Inlet Tempe	rature	Turbi	ne Inlet Tempe	rature
Parameter	35° F	75° F	95° F	35° F	75° F	95° F
Formaldehyde (CH ₂ O)						
CH 2 O (lb/hr) = CH 2 O (ppm actual)	x Volume flow (a	cfm) x 30 (mole	wat CH - O) x 21	16.8 lb/ft ² (press	sure) /	
Ciry C (ishin) Ciry C (ppin actual)	x voidino non (d		as constant, R) x			
CH 2 O (ppm actual) = CH 2 O (ppmo	1 @ 15%() ~ \ v [/2				// × 00 11111/11	
Oxygen (%, dry)(O_2 dry) = Oxygen	-		.U.U = 10/J X (1-10)	0/3/2/00/		
Basis, ppm actual- calculated	0.105	0.102	0.102	0.122	0.117	0.115
	0.105	0.102	0.091	0.122	0.091	0.113
CT, ppmvd @15% O ₂		0.00		-,		
Moisture (%)	8.05	9.16	10.62	11.71	12.50	13.29
Oxygen (%)	12.40	12.34	12.09	10.53	10.70	10.68
Oxygen (%) dry	13.49	13.58	13.53	11.93	12.23	12.32
Exhaust Flow (acfm)	2,859,044	2,806,249	2,699,692	2,726,718	2,842,493	2,758,200
Exhaust Temperature (°F)	1,098	1,117	1,132	1,107	1,106	1,118
Molecular weight	28.42	28.30	28.13	28.31	28.20	28.10
CT Emission rate (lb/hr)	0.450	0.423	0.398	0.494	0.491	0.462
Heat Input (MMBtu/hr, HHV)	2,209	2,090	1,975	2,260	2,260	2,134
CT Emission rate (lb/10 ¹² Btu) (HHV)	203.6	202.5	201.4	218.4	217.3	216.7
CT Emission rate (lb/10 ⁶ Btu) (HHV)	2.04E-04	2.03E-04	2.01E-04	2.18E-04	2.17E-04	2.17E-04

Note: ppmvd= parts per million, volume dry; O₂= oxygen.

Source: General Electric Company, 2013 (CT Performance Data); Golder, 2013



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Table GE-A-7: Hazardous Air Pollutant Emissions for Additional Emission Units - ULSD Oil Firing (GE 7FA.05)

			Annual Emission Basis
Parameter	Units	Value	Black Start Diesel Engines
Number			4
Heat Input Rate	MMBtu/hr	per unit	29.01
Maximum operation/yr	hours	per unit	100
Heat Input Rate/annual	MMBtu/yr	all units	11,603
HAPs [Section 112(b) of Clean Air Act]	Emissio	n Factor ^{a, b}	Emissions (TPY)
Acrolein	lb/MMBtu	7.88E-06	4.57E-05
Acetaldehyde	lb/MMBtu	2.52E-05	1.46E-04
Benzene	lb/MMBtu	7.76E-04	4.50E-03
Formaldehyde	lb/MMBtu	7.89E-05	4.58E-04
Naphthalene	lb/MMBtu	1.30E-04	7.54E-04
Toluene	lb/MMBtu	2.81E-04	1.63E-03
Xylene	ib/MMBtu	1.93E-04	1.12E-03
Acenaphthene	lb/MMBtu	4.68E-06	2.72E-05
Acenaphthylene	lb/MMBtu	9.23E-06	5.35E-05
Anthracene	lb/MMBtu	1.23E-06	7.14E-06
Benzo(a)anthracene	lb/MMBtu	6.22E-07	3.61E-06
Benzo(b)fluoranthene	lb/MMBtu	1.11E-06	6.44E-06
Benzo(k)fluoranthene	lb/MMBtu	2.18E-07	1.26E-06
Benzo(g,h,i)perylene	lb/MMBtu	5.56E-07	3.23E-06
Benzo(g)n,n)perylene Benzo(a)pyrene	Ib/MMBtu	2.57E-07	1.49E-06
Chrysene	Ib/MMBtu	1.53E-06	8.88E-06
Dibenzo(a,h)anthracene			
Fluoanthene	Ib/MMBtu	3.46E-07	2.01E-06
	Ib/MMBtu	4.03E-06	2.34E-05
Fluorene	Ib/MMBtu	4.47E-06	2.59E-05
Indo(1,2,3-cd)pyrene	lb/MMBtu	4.14E-07	2.40E-06
Phenanthrene	lb/MMBtu	1.05E-06	6.09E-06
Pyrene	lb/MMBtu	3.71E-06	2.15E-05
Arsenic	lb/10 ¹² Btu	4.0	2.32E-05
Beryllium	lb/10 ¹² Btu	3.0	1.74E-05
Cadmium	lb/10 ¹² Btu	3.0	1.74E-05
Chromium	Ib/10 ¹² Btu	3.0	1.74E-05
Lead	lb/10 ¹² Btu	9.0	5.22E-05
	lb/10 ¹² Btu		
Mercury		3.0	1.74E-05
Manganese	lb/10 ¹² Btu	6.0	3.48E-05
Nickel	lb/10 ¹² Btu	3.0	1.74E-05
Selenium	lb/10 ¹² Btu	15.0	8.70E-05
Total HAPs =			9.13E-03
Max. Individual HAP =			4.50E-03

^a EPA AP-42, Section 3.4, Large Stationary Diesel And All Stationary Dual-fuel Engines (October 1996)



^b EPA AP-42, Section 1.3, Fuel Oil Combustion for metals (September 1998).

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Table GE-A-8: Greenhouse Gas (GHG) Emissions GE 7FA.05, Base Load

	Maxir Heat Inpu (MMB	t at 75 °F	Emission (lb/MM		Hourly GHG (lb/l		Operation Natural	ng Hours Distillate	Annual GHG		CO₂e Emis		CO₂e Natural	Emission (TPY) Distillate	Rate ^b
Pollutant	Natural Gas	Oil	Natural Gas	Fuel Oil	Natural Gas	Fuel Oil	Gas	Fuel Oil	Naturai Gas	Fuel Oil	Natural Gas	Fuel Oil	Gas	Fuel Oil	Total
Natural Gas On										_					
CO⁵	2,090.2	0.0	116.9	163.0	244,257.4	0.0	3,390	0	414,016.2	0	244,257.4	0.0	414,016.2	0	414,016.2
CH₄	2,090.2	0.0	0.002204	0.006612	4.6	0.0	3,390	0	7.8	0	96.7	0.0	164.0	0	164.0
N₂O	2,090.2	0.0	0.0002204	0.001322	0.5	0.0	3,390	0	0.8	0	142.8	0.0	242.1	0	242.1
										Total	244,496.9	0.0	414,422.3	0.0	414,422.3
Natural Gas & [Distillate Fuel Oil														
CO₂	2,090.2	2,260.3	116.9	163.0	244,257.4	368,451.5	2,890	500	352,951.9	92,112.9	244,257.4	368,451.5	352,951.9	92,112.9	445,064.8
CH₄	2,090.2	2,260.3	0.002204	0.006612	4.6069	14.9453	2,890	500	6.7	3.7	96.7	313.9	139.80	78.46	218.3
N ₂ O	2,090.2	2,260.3	0.0002204	0.001322	0.4607	2.9891	2,890	500	0.7	0.7	142.8	926.6	206.37	232	438.0
_	,									Total	244,496.9	369,692.0	353,298.1	92,423.0	445,721.1
									Ma	aximum Total			414,422.3	92,423.0	445,721.1

Table C-2, Subpart C, 40 CFR 98. Emission factors in kg/MMBtu

Pollutant	Natural Gas	Distillate Fuel Oil
CO ₂	53.02	73.96
CH₄	0.001	0.003
N₂O	0.0001	0.0006

Conversion factor from kg/MMBtu to lb/MMBtu: 2.204

^b CH₄ and N₂O are multiplied by CO₂e factor

Pollutant	CO _{2e} Factor
CH₄	21
N₂O	310





Table GE-A-9: Greenhouse Gas (GHG) Emissions for Additional Emission Units

Emission Unit/ Pollutant	Maximum Heat Input (MMBtu/hr)	Emission Factor ^a (lb/MMBtu)	Hourly GHG Emissions (lb/hr)	Operating Hours	Annual GHG Emissions (TPY)	-	ns Rate (TPY) ^b er of Units
Black Start Diesel En	gine (No. Units)					1	4
CO2	29	163.0	4,728.4	100	236.4	236.4	945.7
CH₄	29	0.006612	0.192	100	0.010	0.20	0.8
N₂O	29	0.001322	0.038	100	0.0019	0.59 237.2	2.4 948.9
Fire Pump Engine							
CO ₂	2.37	163.0	386.0	100	19.3	19.3	
CH₄	2.37	0.006612	0.016	100	0.001	0.02	
N₂O	2.37	0.001322	0.003	100	0.0002	0.05 19.4	

^a Table C-2, Subpart C, 40 CFR 98. Emission factors in kg/MMBtu

_	Pollutant	Natural Gas	Distillate Fuel Oil
	CO ₂	53.02	73.96
	CH₄	0.001	0.003
	N ₂ O	0.0001	0.0006

Conversion factor from kg/MMBtu to lb/MMBtu:

2.204

^b CH₄ and N₂O are multiplied by CO₂e factor

	Pollutant	CO _{2e} Factor	
_	CH₄	21	
	N_2O	310	







Table GE-A-10: Comparison of GE7FA.04 and GE7FA.05 Performance Emissions - Simple Cycle Operation (GE 7FA.04 vs GE 7FA.05) Dry Low NO_X Combustor, ULSD Oil and Natural Gas

		CT Only - ISC) Conditions	
	GE7	FA.04		FA.05
Parameter	Fuel Oil 59 °F	Nature Gas 59 °F	Fuel Oil 59 °F	Nature Gas 59 °F
Combustion Turbine Performance				
Heat Input (MMBtu/hr, LHV)	1,926.2	1,657.0	2,121.6	1,913.9
Heat Input (MMBtu/hr, HHV)	2,052.4	1,839.1	2,260.6	2,124.2
Evaporative Cooler	None	None	None	None
Relative Humidity (%)	60	60	60	60
Fuel heating value (Btu/lb, LHV)	18,300	21,515	18,300	21,515
Fuel heating value (Btu/lb, HHV)	19,499	23,879	19,499	23,879
Ratio of fuel heating values (HHV/LHV)	1.066	1.110	1.066	1.110
Heat Content (Btu/lb, LHV) Fuel Usage (lb/hr) Heat Content (Btu/cf, LHV) Fuel Density (lb/ft³) Fuel Usage (cf/hr)	18,300 105,257 918 0.0502 2,098,255	21,515 77,017 918 0.0427 1,805,031	18,300 115,934 918 0.0502 2,311,112	21,515 88,957 918 0.0427 2,084,870
• , ,	, ,	, .	, ,	
Steady-state Emissions (ISO Conditions) NOx corrected to 15% O2 (ppmvd) NOx as NO2 (lb/hr)	42 328	9 60	42 369	9 69
NOx corrected to 15% O2 (ppmvd) NOx as NO2 (lb/hr)			•—	
NOx corrected to 15% O2 (ppmvd) NOx as NO2 (lb/hr) CO (ppmvd)	328	60	369	69
NOx corrected to 15% O2 (ppmvd) NOx as NO2 (lb/hr) CO (ppmvd) CO (lb/hr)	328 20	60 9	369 20	69 9
NOx corrected to 15% O2 (ppmvd) NOx as NO2 (lb/hr) CO (ppmvd)	328 20 65	60 9 29	369 20 72	69 9 33



APPENDIX B EXPECTED PERFORMANCE AND EMISSION INFORMATION FOR SIEMENS F5 CTS

July 2013 133-87588

Table S-B-1: Design Information and Stack Parameters - Simple Cycle Operation Low NO $_{\rm X}$ Combustion, Natural Gas Siemens F5

			CT	Only			
	Base Load	d Turbine Inlet To	emperature	40% Load 1 Tempe	44% Load Turbine Inlet Temperature		
Parameter	35°F	75°F	95°F	35°F	75°F	95°F	
Combustion Turbine Performance							
Heat Input (MMBtu/hr, LHV)	2,022	2,068	1,933	1,114	1,107	1,108	
Heat Input (MMBtu/hr, HHV)	2,246	2,297	2,147	1,237	1,229	1,230	
Evaporative Cooler	ÓFF	ÓFF	OFF	ÓFF	ÓFF	ÓFF	
Relative Humidity (%)	60	60	60	60	60	60	
Fuel heating value (Btu/lb, LHV)	20.982	20,982	20,982	20.982	20.982	20,982	
Fuel heating value (Btu/lb, HHV)	23,299	23,299	23,299	23,299	23,299	23,299	
Ratio of fuel heating values (HHV/LHV)	1.110	1.110	1.110	1.110	1.110	1,110	
CT Exhaust Flow							
Volume flow (acfm) = [Mass flow (lb/hr) x 1545.4 >	: Temp (°F + 460 K)] / [2						
Mass Flow (lb/hr)	4,287,739	4,576,438	4,278,422	2,785,192	2,732,374	2,693,628	
Temperature (°F)	1,107	1,108	1,127	1,118	1,154	1,176	
Moisture (% Vol.)	8.23	9.20	10.67	7.09	8.44	10.02	
Oxygen (% Vol.)	12.19	12.28	12.01	13.45	13.12	12.74	
Molecular Weight	28.42	28.30	28.13	28.49	28.34	28.17	
Volume flow (acfm)	2,882,874	3,091,716	2,942,724	1,880,866	1,897,022	1,907,287	
Fuel Usage							
Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000							
Heat Input (MMBtu/hr, LHV)	2,022	2,068	1,933	1,114	1,107	1,108	
Heat Content (Btu/lb, LHV)	20,982	20,9B2	20,982	20,982	20,982	20,982	
Fuel Usage (lb/hr)	96,368	98,561	92,127	53,093	52,760	52,807	
Heat Content (Stu/cf, LHV)	918	918	918	918	918	918	
Fuel Density (lb/ft ³)	0.0438	0.0438	0.0438	0.0438	0.0438	0.0438	
Fuel Usage (cf/hr)	2,202,614	2,252,723	2,105,664	1,213,508	1,205,882	1,206,972	
CT Stack Parameters							
Stack Height (feet)	80	80	80	80	80	80	
Stack Diameter (feet)	23	23	23	23	23	23	
CT Stack Flow Conditions Velocity (ft/sec) = Volume flow (acfm) / [((diameter	·\² /4\ v 3 141591 / 60 se	c/min					
Stack Temperature (°F)	1.107	1,108	1,127	1.118	1.154	1.176	
Volume flow (acfm)	2,882,874	3.091.716	2.942.724	1.880.866	1,897,022	1,907,287	
Diameter (feet)	2,002,074	23	2,942,724	23	1,097,022	1,907,267	
Velocity (ft/sec)- calculated	23 115.6	124.0	∠3 118.0	75.5	23 76.1	76.5	
velocity (ivsec)- calculated	115,6	124.0	110.0	15.5	70.1	70.5	

Note: Universal gas constant = 1,545.4 ft-lb(force)/°R; atmospheric pressure = 2,112.5 lb(force)/ft² (@14.67 psia).

Source: Siemens, 2013





Table S-B-2: Maximum Emissions for Criteria Pollutants - Simple Cycle Operation NO_x Combustion, Natural Gas, Base Load Siemens F5

	CT Only						
	Base Load	Turbine Inlet T		40% Load T		44% Load Turbine Inlet Temperature	
Parameter	35°F	75°F	95°F	35°F	75°F	95°F	
Particulate Matter (PM10/PM2.5)							
PM ₁₀ /PM _{2.5} (lb/hr) = PM Emissions Rate (lb/hr) (front-half & back-ha	alf)						
PM ₁₀ /PM _{2.5} Emission Rate (lb/hr)	9	10	9	8	8	8	
0 K B: :1 (00)							
Sulfur Dioxide (SO ₂)							
SO ₂ (lb/hr)= Natural gas (scf/hr) x sulfur content(gr/100 scf) x 1 lb/7		,	0.405.004	4 040 500	4 005 000		
Fuel Use (scf/hr)	2,202,614	2,252,723	2,105,664	1,213,508	1,205,882	1,206,972	
Sulfur Content (grains/ 100 cf)	2	2	2	2	2	2	
ib SO ₂ /lb S (64/32)	2	2	2	2	2	2	
SO ₂ Emission Rate (lb/hr)	12.6	12.9	12.0	6.9	6.9	6.9	
	NA	NA	NA	NA	NA	NA	
SO ₂ (lb/hr)= SO ₂ Emissions Rate (lb/MMBtu) x Heat Input (MMBtu/	hr, HHV)						
SO ₂ Emission Rate (lb/MMBtu)	0.0056	0.0056	0.0056	0.0056	0.0056	0.0056	
Heat Input (MMBtu/hr, HHV)	2,246	2,297	2,147	1,237	1,229	1,230	
SO ₂ Emission Rate (lb/hr) Nitrogen Oxides (No.)	12.6	12.9	12.0	6.9	6.9	6.9	
Nitrogen Oxides (No.) NO $_{\times}$ (ppmv actual) = NO $_{\times}$ (ppmd @ 15%O $_{2}$) x [(20.9 - O $_{2}$ dry)/(20 Oxygen (%, dry)(O $_{2}$ dry) = Oxygen (%)/[1-Moisure (%)] NO $_{\times}$ (lb/hr) = NO $_{\times}$ (ppm actual) x Volume flow (acfm) x 46 (mole. w	.9 - 15)] x [1- Mois gt NO _x) x 2112.5	sture(%)/100] lb/ft² (pressure) / [1545.4 ft-lb (gas constant, R)	x Actual Tem	p. (°R)] x 60 m	
Nitrogen Oxides (No _x) NO _x (ppmv actual) = NO _x (ppmd @ 15%O ₂) x [(20.9 - O ₂ dry)/(20 Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)] NO _x (lb/hr) = NO _x (ppm actual) x Volume flow (acfm) x 46 (mole. w. Basis, ppm actual	.9 - 15)] x [1- Mois gt NO _x) x 2112.5 10.7	sture(%)/100] lb/ft ² (pressure 10.2) / [1545.4 ft-lb (gas constant, R) 9.1	x Actual Tem 9.2	p. (°R)] x 60 m 9.3	
Nitrogen Oxides (No _x) NO _x (ppmv actual) = NO _x (ppmd @ 15%O ₂) x [(20.9 - O ₂ dry)/(20 Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)] NO _x (b/hr) = NO _x (ppm actual) x Volume flow (acfm) x 46 (mole. w. Basis, ppm actual NO _x , ppmvd @15% O ₂ (15 ppmvd)	.9 - 15)] x [1- Mois gt NO _x) x 2112.5 10.7 9	sture(%)/100] lb/ft² (pressure 10.2 9) / [1545.4 ft-lb (10.2 9	gas constant, R) 9.1 9	x Actual Tem 9.2 9	р. (°R)] x 60 п 9.3 9	
Nitrogen Oxides (No _x) NO _x (ppmv actual) = NO _x (ppmd @ 15%O ₂) x [(20.9 - O ₂ dry)/(20 Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)] NO _x (lb/hr) = NO _x (ppm actual) x Volume flow (acfm) x 46 (mole. w. Basis, ppm actual NO _x , ppmvd @15% O ₂ (15 ppmvd) Moisture (%)	.9 - 15)] x [1- Mois gt NO _x) x 2112.5 10.7 9 8.23	sture(%)/100] lb/ft² (pressure 10.2 9 9.20) / [1545.4 ft-lb (10.2 9 10.67	gas constant, R) 9.1 9 7.09	x Actual Tem 9.2 9 8.44	p. (°R)] x 60 m 9.3 9 10.02	
Nitrogen Oxides (No _x) NO _x (ppmv actual) = NO _x (ppmd @ 15%O ₂) x [(20.9 - O ₂ dry)/(20 Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)] NO _x (lb/hr) = NO _x (ppm actual) x Volume flow (acfm) x 46 (mole. w. Basis, ppm actual NO _x , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%)	.9 - 15)] x [1- Mois gt NO _x) x 2112.5 10.7 9 8.23 12.19	sture(%)/100] /b/ft ² (pressure 10.2 9 9.20 12.28) / [1545.4 ft-lb (10.2 9 10.67 12.01	gas constant, Rj 9.1 9 7.09 13.45	x Actual Tem 9.2 9 8.44 13.12	p. (°R)] x 60 m 9.3 9 10.02 12.74	
Nitrogen Oxides (No.) NO $_x$ (ppmv actual) = NO $_x$ (ppmd @ 15%O $_2$) x [(20.9 - O $_2$ dry)/(20 Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure (%)] NO $_x$ (lb/hr) = NO $_x$ (ppm actual) x Volume flow (acfm) x 46 (mole. w. Basis, ppm actual) NO $_x$, ppmvd @15% O $_2$ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) dry	.9 - 15)] x [1- Mois gt NO _x) x 2112.5 10.7 9 8.23 12.19 13.28	sture(%)/100] lb/ft ² (pressure 10.2 9 9.20 12.28 13.52) / [1545.4 ft-lb (: 10.2 9 10.67 12.01 13.44	gas constant, R) 9.1 9 7.09 13.45 14.48	9.2 9.2 9 8.44 13.12 14.33	p. (°R)] x 60 m 9.3 9 10.02 12.74 14.16	
Nitrogen Oxides (No _x) NO _x (ppmv actual) = NO _x (ppmd @ 15%O ₂) x [(20.9 - O ₂ dry)/(20 Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)] NO _x (lb/hr) = NO _x (ppm actual) x Volume flow (acfm) x 46 (mole. w. Basis, ppm actual NO _x , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) Oxygen (%)	.9 - 15)] x [1- Mois gt NO _x) x 2112.5 10.7 9 8.23 12.19 13.28 2,882,874	sture(%)/100] lb/ft ² (pressure 10.2 9 9.20 12.28 13.52 3,091,716	0) / [1545.4 ft-lb (10.2 9 10.67 12.01 13.44 2,942,724	gas constant, R) 9.1 9 7.09 13.45 14.48 1,880,866	9.2 9 8.44 13.12 14.33 1,897,022	p. (°R)] x 60 m 9.3 9 10.02 12.74 14.16 1,907,287	
Nitrogen Oxides (No _x) NO _x (ppmv actual) = NO _x (ppmd @ 15%O ₂) x [(20.9 - O ₂ dry)/(20 Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)] NO _x (lb/hr) = NO _x (ppm actual) x Volume flow (acfm) x 46 (mole. w. Basis, ppm actual NO _x , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) Flow (acfm) Flow (acfm)	.9 - 15)] x [1- Mois gt NO _x) x 2112.5 10.7 9 8.23 12.19 13.28 2,882,874 2,645,613	sture(%)/100] lb/ft² (pressure 10.2 9 9.20 12.28 13.52 3,091,716 2,807,278	10.2 9 10.67 12.01 13.44 2,942,724 2,628,735	gas constant, R) 9.1 9 7.09 13.45 14.48 1,880,866 1,747,513	9.2 9 8.44 13.12 14.33 1,897,022 1,736,914	p. (°R)] x 60 π 9.3 9 10.02 12.74 14.16 1,907,287 1,716,177	
Nitrogen Oxides (No _x) NO _x (ppmv actual) = NO _x (ppmd @ 15%O ₂) x [(20.9 - O ₂ dry)/(20 Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)] NO _x (lb/hr) = NO _x (ppm actual) x Volume flow (acfm) x 46 (mole. w. Basis, ppm actual NO _x , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) Flow (acfm) Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F)	gt NO _x) x [1- Mois gt NO _x) x 2112.5 1 10.7 9 8.23 12.19 13.28 2,882,874 2,645,613 1,107	sture(%)/100] lb/ft² (pressure 10.2 9 9.20 12.28 13.52 3.091,716 2,807,278 1,108	10.2 9 10.67 12.01 13.44 2,942,724 2,628,735 1,127	gas constant, R) 9.1 9 7.09 13.45 14.48 1,880,866 1,747,513 1,118	9.2 9 8.44 13.12 14.33 1,897,022	ρ. (°R)] x 60 π 9.3 9 10.02 12.74 14.16 1,907,287	
Nitrogen Oxides (No _x) NO _x (ppmv actual) = NO _x (ppmd @ 15%O ₂) x [(20.9 - O ₂ dry)/(20 Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)] NO _x (lb/hr) = NO _x (ppm actual) x Volume flow (acfm) x 46 (mole. w. Basis, ppm actual NO _x , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) dry Flow (acfm) Flow (acfm)	9 - 15)] x [1- Mois gt NO _x) x 2112.5 10.7 9 8.23 12.19 13.28 2,882,874 2,645,613 1,107 74.0	sture(%)/100] lb/ft² (pressure 10.2 9 9.20 12.28 13.52 3,091,716 2,807,278	10.2 9 10.67 12.01 13.44 2,942,724 2,628,735 1,127 71.1	gas constant, R) 9.1 9 7.09 13.45 14.48 1,880,866 1,747,513	9.2 9 8.44 13.12 14.33 1,897,022 1,736,914 1,154	p. (°R)] x 60 m 9.3 9 10.02 12.74 14.16 1,907,287 1,716,177 1,176	
Nitrogen Oxides (No _x) NO _x (ppmv actual) = NO _x (ppmd @ 15%O ₂) x [(20.9 - O ₂ dry)/(20 Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)] NO _x (lb/hr) = NO _x (ppm actual) x Volume flow (acfm) x 46 (mole. w. Basis, ppm actual NO _x , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) Oxygen (%) dry Flow (acfm) Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) NO _x Emission Rate (lb/hr)	9 - 15)] x [1- Mois gt NO _x) x 2112.5 10.7 9 8.23 12.19 13.28 2,882,874 2,645,613 1,107 74.0	sture(%)/100] (b/ft² (pressure 10.2 9 9.20 12.28 13.52 3,091,716 2,807,278 1,108 76.0	10.2 9 10.67 12.01 13.44 2,942,724 2,628,735 1,127	gas constant, R) 9.1 9 7.09 13.45 14.48 1,880,866 1,747,513 1,118 40.9	9.2 9 8.44 13.12 14.33 1,897,022 1,736,914 1,154 40.7	p. (°R)] x 60 m 9.3 9 10.02 12.74 14.16 1,907,287 1,716,177 1,176 40.7	
Nitrogen Oxides (No.) NO _x (ppmv actual) = NO _x (ppmd @ 15%O ₂) x [(20.9 - O ₂ dry)/(20 Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)] NO _x (lb/hr) = NO _x (ppm actual) x Volume flow (acfm) x 46 (mole. w. Basis, ppm actual) NO _x , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) Oxygen (%) Oxygen (%) Oxygen (%) dry Flow (acfm) Flow (acfm) Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) NO _x Emission Rate (lb/hr)	gt NO _x) x [1- Mois gt NO _x) x 2112.5 10.7 9 8.23 12.19 13.28 2,882,874 2,645,613 1,107 74.0 77	sture(%)/100] (b/ft² (pressure 10.2 9 9.20 12.28 13.52 3,091,716 2,807,278 1,108 76.0 79	10.2 9 10.67 12.01 13.44 2,942,724 2,628,735 1,127 71.1 74	gas constant, R) 9.1 9 7.09 13.45 14.48 1,880,866 1,747,513 1,118 40.9 42	9.2 9 8.44 13.12 14.33 1,897,022 1,736,914 1,154 40.7 42	p. (°R)] x 60 m 9.3 9 10.02 12.74 14.16 1,907,287 1,716,177 1,176 40.7 42	
Nitrogen Oxides (No _x) NO _x (ppmv actual) = NO _x (ppmd @ 15%O ₂) x [(20.9 - O ₂ dry)/(20 Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)] NO _x (lb/hr) = NO _x (ppm actual) x Volume flow (acfm) x 46 (mole. w. Basis, ppm actual NO _x , ppmvd @15% O ₂ (15 ppmvd) Moisture (%) Oxygen (%) Oxygen (%) Oxygen (%) dry Flow (acfm) Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) NO _x Emission Rate (lb/hr)	9 - 15)] x [1- Mois gt NO _x) x 2112.5 10.7 9 8.23 12.19 13.28 2,882,874 2,645,613 1,107 74.0	sture(%)/100] (b/ft² (pressure 10.2 9 9.20 12.28 13.52 3,091,716 2,807,278 1,108 76.0	10.2 9 10.67 12.01 13.44 2,942,724 2,628,735 1,127 71.1	gas constant, R) 9.1 9 7.09 13.45 14.48 1,880,866 1,747,513 1,118 40.9	9.2 9 8.44 13.12 14.33 1,897,022 1,736,914 1,154 40.7	p. (°R)] x 60 m 9.3 9 10.02 12.74 14.16 1,907,287 1,716,177 1,176 40.7	





Table S-B-2: Maximum Emissions for Criteria Pollutants - Simple Cycle Operation NO_X Combustion, Natural Gas, Base Load Siemens F5

			CT (Only		
	Base Load	Turbine Inlet T	40% Load Turbine Inlet Temperature		44% Load Turbine Inlea Temperature	
Parameter	35°F	75°F	95°F	35°F	75°F	95°F
Carbon Monoxide (CO)						
CO (ppmv wet or actual) = CO (ppmvd @ $15\%O_2$) x [(20.9 - O_2 c	drv)/(20.9 - 15)] x [1-	Moisture(%)/10	001			
Oxygen (%, dry)(O 2 dry) = Oxygen (%)/[1-Moisure (%)]	27 (-,			
CO (lb/hr) = CO (ppm actual) x Volume flow (acfm) x 28 (mole. wc	of COL v 2112 5 lb/ft ²	(nressure) / [1	545 4 ft-lh (cas i	constant R) v A	ctual Tomn (°	R)1 v 60 min/h
Basis, ppm actual	4.74	4.54	4.52	9.10	9.18	9.25
Basis, ppmvd	NA	NA	NA	NA	NA NA	NA
Basis, ppmvd @ 15% O ₂	4	4	4	9	9	9
Moisture (%)	8.23	9.20	10.67	7.09	8.44	10.02
Oxygen (%)	12.19	12.28	12.01	13.45	13.12	12.74
Oxygen (%) dry	13.28	13.52	13.44	14.48	14.33	14.16
Flow (acfm)	2,882,874	3,091,716	2,942,724	1,880,866	1,897,022	1,907,287
Flow (acfm), dry	2.645.613	2,807,278	2,628,735	1,747,513	1,736,914	1,716,177
Exhaust Temperature (°F)	1,107	1.108	1,127	1,118	1,154	1,176
CO Emission Rate (lb/hr)	20.0	20.6	19.2	24.9	24.8	24.8
20 Limbolott Nato (Ibrilly	21	21	20	26	26	26
CO (lb/hr) = CO Emissions Rate (lb/MMBtu) x Heat Input (MMBtu				20		20
CO Emission Rate (lb/MMBtu)	0.0093	0.0091	0.0093	0.0210	0.0212	0.0211
Heat Input (MMBtu/hr, HHV)	2246	2297	2147	1237	1229	1230
CO Emission Rate (lb/hr)	21.0	21.0	20.0	26.0	26.0	26.0
Volatile Organic Compounds (VOC)						
) ₂ dry)/(20.9 - 15)] x	[1- Moisture(%)/100]			
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure (%)]						
Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)]				(gas constant, R	?) x Actual Ten	np. (°R)] x 60
Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)]				(gas constant, R 1.01	r) x Actual Ten 1.02	np. (°R)] x 60 1.03
Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)] VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfm) x 16 (mole.	wgt CH ₄) x 2112.5	lb/ft² (pressure) / [1545.4 ft-lb			
Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure (%)] VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfm) x 16 (mole. Basis, ppm actual	wgt CH ₄) x 2112.5 . 1.18	lb/ft² (pressure 1.14) / [1545.4 ft-lb 1.13	1.01	1.02	1.03
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure (%)] VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfm) x 16 (mole. Basis, ppm actual Basis, ppmvd @ 15% O_2	wgt CH ₄) x 2112.5 i 1.18 1	<i>lb/f</i> t² (pressure 1.14 1) / [1 <i>545.4 ft-lb</i> 1.13 1	1.01 1	1.02 1	1.03 1
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure (%)] VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfm) x 16 (mole. Basis, ppm actual Basis, ppmvd @ 15% O_2 Moisture (%)	wgt CH ₄) x 2112.5 a 1.18 1 8.23	<i>lb/ft² (pressure</i> 1.14 1 9.20	1,13 1,13 1 10.67	1.01 1 7.09	1.02 1 8.44	1.03 1 10.02
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure (%)] VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfm) x 16 (mole. Basis, ppm actual Basis, ppmvd @ 15% O_2 Moisture (%) Oxygen (%) wet	wgt CH ₄) x 2112.5 ; 1.18 1 8.23 12.19	lb/ft ² (pressure 1.14 1 9.20 12.28	1.13 1.13 1 10.67 12.01	1.01 1 7.09 13.45	1.02 1 8.44 13.12	1.03 1 10.02 12.74 14.16
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure (%)] VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfm) x 16 (mole. Basis, ppm actual Basis, ppmvd @ 15% O $_2$ Moisture (%) Oxygen (%) wet Oxygen (%) dry	wgt CH ₄) x 2112.5 ; 1.18 1 8.23 12.19 13.28	lb/ft ² (pressure 1.14 1 9.20 12.28 13.52) / [1545.4 ft-lb 1.13 1 10.67 12.01 13.44	1.01 1 7.09 13.45 14.48	1.02 1 8.44 13.12 14.33	1.03 1 10.02 12.74 14.16 1,907,287
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure (%)] VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfm) x 16 (mole. Basis, ppm actual Basis, ppmvd @ 15% O $_2$ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm)	wgt CH ₄) x 2112.5 d 1.18 1 8.23 12.19 13.28 2,882,874	/b/ft ² (pressure 1.14 1 9.20 12.28 13.52 3,091,716	1.13 1.067 12.01 13.44 2,942,724	1.01 1 7.09 13.45 14.48 1,880,866	1.02 1 8.44 13.12 14.33 1,897,022	1.03 1 10.02 12.74
Oxygen (%, dry)(O 2 dry) = Oxygen (%)/[1-Moisure (%)] VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfm) x 16 (mole. Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry	wgt CH ₄) x 2112.5 x 1.18 1 8.23 12.19 13.28 2,882,874 2,645,613 1,107 2.4	hb/ft² (pressure 1.14 1 9.20 12.28 13.52 3,091,716 2,807,278	1.13 1.0.67 12.01 13.44 2,942,724 2,628,735 1,127 2.4	1.01 1 7.09 13.45 14.48 1,880,866 1,747,513 1,118 1.6	1.02 1 8.44 13.12 14.33 1,897,022 1,736,914 1,154 1.5	1.03 1 10.02 12.74 14.16 1,907,287 1,716,177 1,176
Oxygen (%, dry)(O 2 dry) = Oxygen (%)/[1-Moisure (%)] VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfm) x 16 (mole. Basis, ppm actual Basis, ppmvd @ 15% O2 Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F)	wgt CH ₄) x 2112.5 x 1.18 1 8.23 12.19 13.28 2,882,874 2,645,613 1,107	hb/ft² (pressure 1.14 1 9.20 12.28 13.52 3,091,716 2,807,278 1,108	1.13 1.0.67 12.01 13.44 2,942,724 2,628,735 1,127	1.01 1 7.09 13.45 14.48 1,880,866 1,747,513 1,118	1.02 1 8.44 13.12 14.33 1,897,022 1,736,914 1,154	1.03 1 10.02 12.74 14.16 1,907,287 1,716,177
Oxygen (%, dry)(O 2 dry) = Oxygen (%)/[1-Moisure (%)] VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfm) x 16 (mole. Basis, ppm actual Basis, ppmvd @ 15% O2 Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) as methane	wgt CH ₄) x 2112.5 x 1.18 1 8.23 12.19 13.28 2,882,874 2,645,613 1,107 2.4	lb/ft² (pressure 1.14 1 9.20 12.28 13.52 3,091,716 2,807,278 1,108 2.6	1.13 1.0.67 12.01 13.44 2,942,724 2,628,735 1,127 2.4	1.01 1 7.09 13.45 14.48 1,880,866 1,747,513 1,118 1.6	1.02 1 8.44 13.12 14.33 1,897,022 1,736,914 1,154 1.5	1.03 1 10.02 12.74 14.16 1,907,287 1,716,177 1,176 1.5
Oxygen (%, dry)(O 2 dry) = Oxygen (%)/[1-Moisure (%)] VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfm) x 16 (mole. Basis, ppm actual Basis, ppmvd @ 15% O2 Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) as methane	wgt CH ₄) x 2112.5 x 1.18 1 8.23 12.19 13.28 2,882,874 2,645,613 1,107 2.4 3.0	hb/ft² (pressure 1.14 1 9.20 12.28 13.52 3,091,716 2,807,278 1,108 2.6 3.1	1.13 1.0.67 12.01 13.44 2,942,724 2,628,735 1,127 2.4	1.01 1 7.09 13.45 14.48 1,880,866 1,747,513 1,118 1.6	1.02 1 8.44 13.12 14.33 1,897,022 1,736,914 1,154 1.5	1.03 1 10.02 12.74 14.16 1,907,287 1,716,177 1,176 1.5
Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) as methane Sulfuric Acid Mist (SAM) Sulfuric Acid Mist (lb/hr)= SO ₂ Emission Rate (lb/hr) x Conversio	wgt CH ₄) x 2112.5 x 1.18 1 8.23 12.19 13.28 2,882,874 2,645,613 1,107 2.4 3.0	b/ft² (pressure 1.14 1 9.20 12.28 13.52 3,091,716 2,807,278 1,108 2.6 3.1) / [1545.4 ft-lb 1.13 1 10.67 12.01 13.44 2,942,724 2,628,735 1,127 2.4 2.9	1.01 1 7.09 13.45 14.48 1,880,866 1,747,513 1,118 1.6 1.6	1.02 1 8.44 13.12 14.33 1,897,022 1,736,914 1,154 1.5 1.6	1.03 1 10.02 12.74 14.16 1,907,287 1,716,177 1,176 1.5 1.6
Oxygen (%, dry)(O 2 dry) = Oxygen (%)/[1-Moisure (%)] VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfm) x 16 (mole. Basis, ppm actual Basis, ppmvd @ 15% O2 Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) as methane Sulfuric Acid Mist (SAM)	wgt CH ₄) x 2112.5 x 1.18 1 8.23 12.19 13.28 2,882,874 2,645,613 1,107 2.4 3.0	hb/ft² (pressure 1.14 1 9.20 12.28 13.52 3,091,716 2,807,278 1,108 2.6 3.1	1.13 1.0.67 12.01 13.44 2,942,724 2,628,735 1,127 2.4	1.01 1 7.09 13.45 14.48 1,880,866 1,747,513 1,118 1.6	1.02 1 8.44 13.12 14.33 1,897,022 1,736,914 1,154 1.5	1.03 1 10.02 12.74 14.16 1,907,287 1,716,177 1,176

Note: ppmvd= parts per million, volume dry; O₂= oxygen.

Source: Siemens, 2013





Table S-B-3: Design Information and Stack Parameters - Simple Cycle Operation Low NO_X Combustion, ULSD Oil, Base Load Siemens F5

			CT (Only		
	Base Load	l Turbine Inlet Te	mperature	50% Load	Turbine Inlet Te	mperature
<u>Par</u> ameter	35°F	75°F	95°F	35°F	75°F	95°F
Combustion Turbine Performance						
Heat Input (MMBtu/hr, LHV)	2,077	2,056	1,930	1,285	1,251	1,190
Heat Input (MMBtu/hr, HHV)	2,216	2,193	2,059	1,371	1,334	1,270
Evaporative Cooler	OFF	OFF	OFF	OFF	OFF	OFF
Relative Humidity (%)	60	60	60	60	60	60
Fuel heating value (Btu/lb, LHV)	18,450	18,450	18,450	18,450	18,450	18,450
Fuel heating value (Btu/lb, HHV)	19,680	19.680	19,680	19.680	19,680	19,680
Ratio of fuel heating values (HHV/LHV)	1.067	1.067	1.067	1.067	1.067	1.067
CT Exhaust Flow						
Volume flow (acfm) = [Mass flow (lb/hr) x 15						
Mass Flow (lb/hr)	4,661,093	4,649,675	4,351,240	3,234,318	3,102,143	2,953,186
Temperature (°F)	1,040	1,067	1,086	1,066	1,112	1,134
Moisture (% Vol.)	6.65	8.38	10.00	5.49	6.85	8.35
Oxygen (% Vol.)	12.64	12.35	12.03	13.59	13.25	12.97
Molecular Weight	28.77	28.58	28.40	28.84	28.70	28.53
Volume flow (acfm)	2,963,172	3,029,221	2,888,125	2,086,449	2,071,671	2,011,508
Fuel Usage						
Fuel usage (lb/hr) = Heat Input (MMBtu/hr)	x 1,000,000 Btu/MN	MBtu [Fuel Heat Co	ontent, Btu/lb (LHV)]		
Heat input (MMBtu/hr, LHV)	2,077	2,056	1,930	1,285	1,251	1,190
Heat content (Btu/lb, LHV)	18,450	18,450	18,450	18,450	18,450	18,450
Fuel usage (lb/hr)	112,575	111,436	104,607	69,648	67,805	64,499
CT Stack Parameters						
Stack Height (feet)	80	80	80	80	80	80
Stack Diameter (feet)	23	23	23	23	23	23
CT Stack Flow Conditions						
Velocity (ft/sec) = Volume flow (acfm) / [((di	ameter)² /4) x 3.141	59] / 60 sec/min				
	1.040	1,067	1,086	1,066	1,112	1,134
	1.070		•	•		
Stack Temperature (°F)	2.963,172	3,029,221	2,888,125	2,086,449	2,071,671	2,011,508
	.,	3,029,221 23	2,888,125 23	2,086,449 23	2,0/1,6/1 23	2,011,508

Note: Universal gas constant = 1,545.4 ft-lb(force)/°R; atmospheric pressure = 2,112.5 lb(force)/ft² (@14.67 psia).







Table S-B-4: Maximum Emissions for Criteria Pollutants - Simple Cycle Operation Low NO_X Combustion, ULSD Oil, Base Load Siemens F5

			CT (Only		
		ad Turbine Inlet Ten			d Turbine Inlet Tem	perature
Parameter	35°F	7 <u>5</u> °F	95°F	35°F	75°F	95°F
Particulate Matter (PM10/PM2.5)						
$PM_{10}/PM_{2.5}$ (lb/hr) = PM Emissions Rate (lb/hr) (from	ont-half & back-half)					
PM ₁₀ /PM _{2.5} Emission Rate (lb/hr)	53	52	48	37	35	33
PM10/PM2.5 (lb/hr) = PM Emissions Rate (lb/MMBt	u) x Heat Input (MMBtu/hr, HH\	0				
PM Emission Rate (lb/MMBtu)	0.024	0.024	0.023	0.027	0.026	0.026
Heat Input (MMBtu/hr, HHV)	2,216	2,193	2,059	1,371	1,334	1,270
PM ₁₀ /PM _{2.5} Emission Rate (lb/hr)	53.0	52.0	48.0	37.0	35.0	33.0
Sulfur Dioxide (SO ₂)						
SO ₂ (lb/hr)= Fuel oil (lb/hr) x sulfur content(% weigi	ht) x (lb SO 2 Ab S) /100					
Fuel oil Sulfur Content	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%	0.0015%
Fuel oil use (lb/hr)	112,575	111,436	104,607	69,648	67,805	64,499
lb SO ₂ / lb S (64/32)	2	2	2	2	2	2
SO ₂ Emission Rate (lb/hr)	3.38	3.3	3.1	2.09	2.0	1.9
CO2 Zimovom nano (iomi)	NA NA	NA	NA NA	NA	NA	NA
SO 2 (lb/hr) = SO 2 Emissions Rate (lb/MMBtu) x He		IVA	IVA	IVA	IVA	INA
SO ₂ Emission Rate (lb/MMBtu) (HHV)	0.0015	0.0015	0.0045	0.0015	0.0045	0.0045
Heat Input (MMBtu/hr, HHV)	2,216		0.0015	0.0015	0.0015	0.0015
, ,		2,193	2,059	1,371	1,334	1,270
SO ₂ Emission Rate (lb/hr)	3.38	3.34	3.14	2.09	2.03	1.93
Nitrogen Oxides (NO.)						
	0.0 O de///20.0 15)] v (1)	Mainture (0/ \ /4.001				
		violsture(76)/100]				
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure	(%)]					
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure NO $_x$ (lb/hr) = NO $_x$ (ppm actual) x Volume flow (acf.	(%)] m) x 46 (mole. wgt NO _x) x 2112	2.5 lb/ft² (pressure) /				
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure NO $_x$ (lb/hr) = NO $_x$ (ppm actual) x Volume flow (acf. Basis, ppm actual	(%)] m) x 46 (mole. wgt NO _x) x 2112 48.9	2.5 lb/ft ² (pressure) / 48.4	48.3	43.9	44.3	44.0
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure NO $_x$ (lb/hr) = NO $_x$ (ppm actual) x Volume flow (acf. Basis, ppm actual NO $_x$, ppmvd @15% O $_2$	(%)] 'm) x 46 (mole. wgt NO _x) x 2112 48.9 42	2.5 lb/ft ² (pressure) / 48.4 42				44.0 42
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure NO $_x$ (lb/hr) = NO $_x$ (ppm actual) x Volume flow (acf. Basis, ppm actual NO $_x$, ppmvd @15% O $_2$ Moisture (%)	(%)] im) x 46 (mole. wgt NO _x) x 2112 48.9 42 6.65	2.5 lb/ft ² (pressure) / 48.4 42 8.38	48.3 42 10.00	43.9 42 5.49	44.3 42 6.85	42 8.35
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure NO $_x$ (lb/hr) = NO $_x$ (ppm actual) x Volume flow (acf. Basis, ppm actual NO $_x$, ppmvd @15% O $_2$ Moisture (%) Oxygen (%)	(%)] im) x 46 (mole. wgt NO _x) x 2112 48.9 42 6.65 12.64	2.5 lb/ft ² (pressure) / 48.4 42 8.38 12.35	48.3 42 10.00 12.03	43.9 42 5.49 13.59	44.3 42 6.85 13.25	42 8.35 12.97
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure NO $_x$ (lb/hr) = NO $_x$ (ppm actual) x Volume flow (acf. Basis, ppm actual NO $_x$, ppm vd @15% O $_2$ Moisture (%) Oxygen (%) Oxygen (%) dry	(%)] m) × 46 (mole. wgt NO _x) × 2112 48.9 42 6.65 12.64 13.54	2.5 lb/ft ² (pressure) / 48.4 42 8.38 12.35 13.48	48.3 42 10.00 12.03 13.37	43.9 42 5.49 13.59 14.38	44.3 42 6.85 13.25 14.22	42 8.35 12.97 14.15
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure NO $_x$ (lb/hr) = NO $_x$ (ppm actual) x Volume flow (acf. Basis, ppm actual NO $_x$, ppmvd @15% O $_2$ Moisture (%) Oxygen (%) Oxygen (%) dry Flow (acfm)	(%)] m) x 46 (mole. wgt NO _x) x 2112 48.9 42 6.65 12.64 13.54 2.963,172	2.5 lb/ft ² (pressure) / 48.4 42 8.38 12.35 13.48 3,029,221	48.3 42 10.00 12.03 13.37 2,888,125	43.9 42 5.49 13.59 14.38 2,086,449	44.3 42 6.85 13.25 14.22 2,071,671	42 8.35 12.97 14.15 2,011,508
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure NO $_x$ (lb/hr) = NO $_x$ (ppm actual) x Volume flow (acf. Basis, ppm actual NO $_x$, ppmvd @15% O $_2$ Moisture (%) Oxygen (%) Oxygen (%) dry Flow (acfm) Flow (acfm), dry	(%)] (m) x 46 (mole. wgt NO _x) x 2112 48.9 42 6.65 12.64 13.54 2,963,172 2,766,121	2.5 lb/ft ² (pressure) / 48.4 42 8.38 12.35 13.48 3,029,221 2,775,372	48.3 42 10.00 12.03 13.37 2,888,125 2,599,313	43.9 42 5.49 13.59 14.38 2,086,449 1,971,903	44.3 42 6.85 13.25 14.22 2,071,671 1,929,762	42 8.35 12.97 14.15 2,011,508 1,843,547
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure NO $_x$ (lb/hr) = NO $_x$ (ppm actual) x Volume flow (acf. Basis, ppm actual NO $_x$, ppmvd @15% O $_2$ Moisture (%) Oxygen (%) Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F)	(%)] (m) x 46 (mole. wgt NO _x) x 2112 48.9 42 6.65 12.64 13.54 2.963,172 2,766,121 1,040	2.5 lb/ft ² (pressure) / 48.4 42 8.38 12.35 13.48 3,029,221 2,775,372 1,067	48.3 42 10.00 12.03 13.37 2,888,125 2,599,313 1,086	43.9 42 5.49 13.59 14.38 2.086,449 1,971,903 1,066	44.3 42 6.85 13.25 14.22 2,071,671 1,929,762 1,112	42 8.35 12.97 14.15 2,011,508 1,843,547 1,134
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure NO $_x$ (lb/hr) = NO $_x$ (ppm actual) x Volume flow (acf. Basis, ppm actual NO $_x$, ppmvd @15% O $_2$ Moisture (%) Oxygen (%) Oxygen (%) dry Flow (acfm), dry	(%)] (m) x 46 (mole. wgt NO _x) x 2112 48.9 42 6.65 12.64 13.54 2,963,172 2,766,121 1,040 364.5	2.5 lb/ft ² (pressure) / 48.4 42 8.38 12.35 13.48 3,029,221 2,775,372 1,067 362.2	48.3 42 10.00 12.03 13.37 2,888,125 2,599,313 1,086 340.2	43.9 42 5.49 13.59 14.38 2.086,449 1,971,903 1,066 226.3	44.3 42 6.85 13.25 14.22 2,071,671 1,929,762 1,112 220.1	42 8.35 12.97 14.15 2,011,508 1,843,547 1,134 209.6
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure NO $_x$ (lb/hr) = NO $_x$ (ppm actual) x Volume flow (acf. Basis, ppm actual NO $_x$, ppmvd @15% O $_2$ Moisture (%) Oxygen (%) Oxygen (%) dry Flow (acfm), dry Exhaust Temperature (°F) NO $_x$ Emission Rate (lb/hr)	(%)] (m) x 46 (mole. wgt NO x) x 2112 48.9 42 6.65 12.64 13.54 2.963,172 2.766,121 1,040 364.5 378	2.5 lb/ft ² (pressure) / 48.4 42 8.38 12.35 13.48 3,029,221 2,775,372 1,067	48.3 42 10.00 12.03 13.37 2,888,125 2,599,313 1,086	43.9 42 5.49 13.59 14.38 2.086,449 1,971,903 1,066	44.3 42 6.85 13.25 14.22 2,071,671 1,929,762 1,112	42 8.35 12.97 14.15 2,011,508 1,843,547 1,134
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure NO_x (Ib/hr) = NO_x (ppm actual) x Volume flow (acf. Basis, ppm actual NO_x , ppmvd @15% O_2 Moisture (%) Oxygen (%) Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) NO_x Emission Rate (Ib/hr) NO_x (Ib/hr) = NO_x Emissions Rate ($Ib/hMBtu$) x Hea	(%)] (m) x 46 (mole. wgt NO _x) x 2112 48.9 42 6.65 12.64 13.54 2.963,172 2.766,121 1,040 364.5 378 at Input (MMBtu/hr, HHV)	2.5 lb/ft ² (pressure) / 48.4 42 8.38 12.35 13.48 3,029,221 2,775,372 1,067 362.2 376	48.3 42 10.00 12.03 13.37 2,888,125 2,599,313 1,086 340.2	43.9 42 5.49 13.59 14.38 2.086,449 1,971,903 1,066 226.3	44.3 42 6.85 13.25 14.22 2,071,671 1,929,762 1,112 220.1	42 8.35 12.97 14.15 2,011,508 1,843,547 1,134 209.6
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure NO_x (lb/hr) = NO_x (ppm actual) x Volume flow (acf. Basis, ppm actual NO_x , ppmvd @15% O_2 Moisture (%) Oxygen (%) Oxygen (%) dry Flow (acfm) Flow (acfm) flow (acfm), dry Exhaust Temperature (°F) NO_x Emission Rate (lb/hr) NO_x (lb/hr) = NO_x Emission Rate ($lb/hMBtu$) x Heal NO_x Emission Rate ($lb/lMBtu$) x Heal x	(%)] (m) x 46 (mole. wgt NO x) x 2112 48.9 42 6.65 12.64 13.54 2.963,172 2.766,121 1,040 364.5 378	2.5 lb/ft ² (pressure) / 48.4 42 8.38 12.35 13.48 3,029,221 2,775,372 1,067 362.2	48.3 42 10.00 12.03 13.37 2,888,125 2,599,313 1,086 340.2	43.9 42 5.49 13.59 14.38 2.086,449 1,971,903 1,066 226.3	44.3 42 6.85 13.25 14.22 2,071,671 1,929,762 1,112 220.1	42 8.35 12.97 14.15 2,011,508 1,843,547 1,134 209.6
NO _x , ppmvd @15% O ₂ Moisture (%) Oxygen (%) Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) NO _x Emission Rate (lb/hr) NO _x (lb/hr) = NO _x Emissions Rate (lb/MMBtu) x Hea	(%)] (m) x 46 (mole. wgt NO _x) x 2112 48.9 42 6.65 12.64 13.54 2.963,172 2.766,121 1,040 364.5 378 at Input (MMBtu/hr, HHV)	2.5 lb/ft ² (pressure) / 48.4 42 8.38 12.35 13.48 3,029,221 2,775,372 1,067 362.2 376	48.3 42 10.00 12.03 13.37 2,888,125 2,599,313 1,086 340.2 353	43.9 42 5.49 13.59 14.38 2.086,449 1,971,903 1,066 226.3 235	44.3 42 6.85 13.25 14.22 2,071,671 1,929,762 1,112 220.1 228	42 8.35 12.97 14.15 2,011,508 1,843,547 1,134 209.6 217







Table S-B-4: Maximum Emissions for Criteria Pollutants - Simple Cycle Operation Low NO_X Combustion, ULSD Oil, Base Load Siemens F5

			CT (
_		ad Turbine Inlet Tem			d Turbine Inlet Tem	
Parameter	35°F	75°F	95°F	35°F	75°F	95°F
Carbon Monoxide (CO)						
CO (ppmv wet or actual) = CO (ppmvd @ 15%O $_2$).		[1- Moisture(%)/100]				
Oxygen (%, dry)(O $_2$ dry) = Oxygen (%)/[1-Moisure ((%)]					
$CO(lb/hr) = CO(ppm actual) \times Volume flow (acfm) :$	x 28 (mole. wgt CO) x 2112.5 lb	/ft ² (pressure) / [154:	5.4 ft-lb (gas constant, l	R) x Actual Temp. (°R)].	x 60 min/hr	
Basis, ppm actual	10.48	10.37	10.34	104.45	105.40	104.83
Basis, ppmvd	NA	NA	NA	NA	NA	NA
Basis, ppmvd @ 15% O ₂	9	9	9	100	100	100
Moisture (%)	6.65	8.38	10,00	5.49	6.85	8.35
Oxygen (%)	12.64	12.35	12.03	13.59	13,25	12.97
Oxygen (%) dry	13.54	13.48	13,37	14.38	14.22	14.15
Flow (acfm)	2,963,172	3,029,221	2,888,125	2,086,449	2,071,671	2,011,508
Flow (acfm), dry	2,766,121	2,775,372	2,599,313	1,971,903	1,929,762	1,843,547
Exhaust Temperature (°F)	1,040	1,067	1,086	1,066	1,112	1,134
CO Emission Rate (lb/hr)	47.5	47.2	44.4	328.0	319.0	303.8
• •	49.0	49.0	46.0	340.0	331.0	315.0
CO (lb/hr) = CO Emissions Rate (lb/MMBtu) x Heat	Input (MMBtu/hr, HHV)					
CO Emission Rate (lb/MMBtu)	0.022	0.022	0.022	0.248	0.248	0.248
Heat Input (MMBtu/hr, HHV)	2,216	2,193	2,059	1,371	1,334	1,270
CO Emission Rate (lb/hr)	49	49	46	340	331	315
	• • •	_				
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi	m) x 16 (mole. wgt CH 4) x 2112			, , , , , , , , , , , , , , , , ,	/2	
Oxygen (%, dry)(O ₂ dry) = Oxygen (%)/[1-Moisure VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual	m) x 16 (mole. wgt CH ₄) x 2112 NA	NA	NA	NA	NA	NA
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂	m) x 16 (mole. wgt CH ₄) x 2112 NA 1	NA 1	NA 1	NA 20	NA 20	20
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O_2 Moisture (%)	m) x 16 (mole. wgt CH ₄) x 211: NA 1 6.65	NA 1 8.38	NA 1 10.00	NA 20 5.49	NA 20 6.85	20 8.35
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet	m) x 16 (mole. wgt CH ₄) x 211; NA 1 6.65 12.64	NA 1 8.38 12.35	NA 1 10.00 12.03	NA 20 5.49 13.59	NA 20 6.85 13.25	20 8.35 12.97
VOC (lb/hr) = VOC (ppm actual) x $Volume$ flow (acfi Basis, ppm actual Basis, $ppmvd$ @ 15% O_2 Moisture (%) Oxygen (%) wet Oxygen (%) dry	m) x 16 (mole. wgt CH ₄) x 211; NA 1 6.65 12.64 13.54	NA 1 8.38 12.35 13.48	NA 1 10.00 12.03 13.37	NA 20 5.49 13.59 14.38	NA 20 6.85 13.25 14.22	20 8.35 12.97 14.15
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm)	m) x 16 (mole. wgt CH ₄) x 211: NA 1 6.65 12.64 13.54 2,963,172	NA 1 8.38 12.35 13.48 3,029,221	NA 1 10.00 12.03 13.37 2,888,125	NA 20 5.49 13.59 14.38 2,086,449	NA 20 6.85 13.25 14.22 2,071,671	20 8.35 12.97 14.15 2,011,508
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry	m) x 16 (mole. wgt CH ₄) x 211: NA 1 6.65 12.64 13.54 2,963,172 2,766,121	NA 1 8.38 12.35 13.48 3,029,221 2,775,372	NA 1 10.00 12.03 13.37 2,888,125 2,599,313	NA 20 5.49 13.59 14.38 2.086.449 1,971,903	NA 20 6.85 13.25 14.22 2,071,671 1,929,762	20 8.35 12.97 14.15 2,011,508 1,843,547
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F)	m) x 16 (mole. wgt CH ₄) x 211: NA 1 6.65 12.64 13.54 2,963,172 2,766,121 1,040	NA 1 8.38 12.35 13.48 3.029,221 2,775,372 1,067	NA 1 10.00 12.03 13.37 2,888,125 2,599,313 1,086	NA 20 5.49 13.59 14.38 2.086,449 1,971,903 1,066	NA 20 6.85 13.25 14.22 2.071,671 1,929,762 1,112	20 8.35 12.97 14.15 2,011,508 1,843,547 1,134
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry	m) x 16 (mole. wgt CH ₄) x 211: NA 1 6.65 12.64 13.54 2,963,172 2,766,121 1,040 2.59	NA 1 8.38 12.35 13.48 3,029,221 2,775,372 1,067 2.60	NA 1 10.00 12.03 13.37 2,888,125 2,599,313 1,086 2.45	NA 20 5.49 13.59 14.38 2,086,449 1,971,903 1,066 35.88	NA 20 6.85 13.25 14.22 2,071,671 1,929,762 1,112 34.59	20 8.35 12.97 14.15 2,011,508 1,843,547 1,134 33.12
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F)	m) x 16 (mole. wgt CH ₄) x 211: NA 1 6.65 12.64 13.54 2,963,172 2,766,121 1,040	NA 1 8.38 12.35 13.48 3.029,221 2,775,372 1,067	NA 1 10.00 12.03 13.37 2,888,125 2,599,313 1,086	NA 20 5.49 13.59 14.38 2.086,449 1,971,903 1,066	NA 20 6.85 13.25 14.22 2.071,671 1,929,762 1,112	20 8.35 12.97 14.15 2,011,508 1,843,547 1,134
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F)	m) x 16 (mole. wgt CH ₄) x 211: NA 1 6.65 12.64 13.54 2,963,172 2,766,121 1,040 2.59	NA 1 8.38 12.35 13.48 3,029,221 2,775,372 1,067 2.60	NA 1 10.00 12.03 13.37 2,888,125 2,599,313 1,086 2.45	NA 20 5.49 13.59 14.38 2,086,449 1,971,903 1,066 35.88	NA 20 6.85 13.25 14.22 2,071,671 1,929,762 1,112 34.59	20 8.35 12.97 14.15 2,011,508 1,843,547 1,134 33.12
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr)	m) x 16 (mole. wgt CH ₄) x 211: NA 1 6.65 12.64 13.54 2,963,172 2,766,121 1,040 2.59 3.1	NA 1 8.38 12.35 13.48 3.029,221 2,775,372 1,067 2.60 3.1	NA 1 10.00 12.03 13.37 2,888,125 2,599,313 1,086 2.45	NA 20 5.49 13.59 14.38 2,086,449 1,971,903 1,066 35.88	NA 20 6.85 13.25 14.22 2,071,671 1,929,762 1,112 34.59	20 8.35 12.97 14.15 2,011,508 1,843,547 1,134 33.12
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr)	m) x 16 (mole. wgt CH ₄) x 211: NA 1 6.65 12.64 13.54 2,963,172 2,766,121 1,040 2.59 3.1	NA 1 8.38 12.35 13.48 3.029,221 2,775,372 1,067 2.60 3.1	NA 1 10.00 12.03 13.37 2,888,125 2,599,313 1,086 2.45	NA 20 5.49 13.59 14.38 2,086,449 1,971,903 1,066 35.88	NA 20 6.85 13.25 14.22 2,071,671 1,929,762 1,112 34.59	20 8.35 12.97 14.15 2,011,508 1,843,547 1,134 33.12
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) Sulfuric Acid Mist (SAM) Sulfuric Acid Mist (lb/hr) = SO ₂ Emission Rate (lb/hr) SO ₂ Emission Rate (lb/hr)	m) x 16 (mole. wgt CH ₄) x 211: NA 1 6.65 12.64 13.54 2.963,172 2.766,121 1.040 2.59 3.1	NA 1 8.38 12.35 13.48 3,029,221 2,775,372 1,067 2.60 3.1	NA 1 10.00 12.03 13.37 2.888,125 2,599,313 1,086 2.45 2.9	NA 20 5.49 13.59 14.38 2.086,449 1,971,903 1,066 35.88 39.0	NA 20 6.85 13.25 14.22 2,071,671 1,929,762 1,112 34.59 37.9	20 8.35 12.97 14.15 2,011,508 1,843,547 1,134 33.12 36.1
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppm vd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) Sulfuric Acid Mist (Ib/hr) = SO ₂ Emission Rate (lb/hr)	m) x 16 (mole. wgt CH ₄) x 211; NA 1 6.65 12.64 13.54 2,963,172 2,766,121 1,040 2.59 3.1 c) x Conversion to H ₂ SO ₄ (% b	NA 1 8.38 12.35 13.48 3,029,221 2,775,372 1,067 2,60 3.1 by weight)/100 3.3	NA 1 10.00 12.03 13.37 2,888,125 2,599,313 1,086 2.45 2.9	NA 20 5.49 13.59 14.38 2.086,449 1,971,903 1,066 35.88 39.0	NA 20 6.85 13.25 14.22 2,071,671 1,929,762 1,112 34.59 37.9	20 8.35 12.97 14.15 2,011,508 1,843,547 1,134 33.12 36.1
VOC (Ib/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) Sulfunc Acid Mist (SAM) Sulfunc Acid Mist (Ib/hr) = SO ₂ Emission Rate (Ib/hr) Conversion to H ₂ SO ₄ (% by weight) SAM Emission Rate (Ib/hr)	m) x 16 (mole. wgt CH_4) x 211: NA 1 6.65 12.64 13.54 2,963,172 2,766,121 1,040 2.59 3.1 c) x Conversion to H_2 SO 4 (% b 3.4	NA 1 8.38 12.35 13.48 3.029,221 2,775,372 1,067 2.60 3.1 by weight)/100 3.3 10	NA 1 10.00 12.03 13.37 2,888,125 2,599,313 1,086 2.45 2.9	NA 20 5.49 13.59 14.38 2.086,449 1,971,903 1,066 35.88 39.0	NA 20 6.85 13.25 14.22 2.071,671 1,929,762 1,112 34.59 37.9	20 8.35 12.97 14.15 2,011,508 1,843,547 1,134 33.12 36.1
VOC (Ib/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) Sulfuric Acid Mist (Ib/hr)= SO ₂ Emission Rate (lb/hr) SO ₂ Emission Rate (lb/hr) Conversion to H ₂ SO ₄ (% by weight) SAM Emission Rate (lb/hr)	m) x 16 (mole. wgt CH_4) x 211: NA 1 6.65 12.64 13.54 2,963,172 2,766,121 1,040 2.59 3.1 r) x Conversion to H_2 SO $_4$ (% b 3.4 10 0.34	NA 1 8.38 12.35 13.48 3.029,221 2.775,372 1,067 2.60 3.1 by weight)/100 3.3 10 0.33	NA 1 10.00 12.03 13.37 2,888,125 2,599,313 1,086 2.45 2.9	NA 20 5.49 13.59 14.38 2.086,449 1,971,903 1,066 35.88 39.0	NA 20 6.85 13.25 14.22 2.071,671 1,929,762 1,112 34.59 37.9	20 8.35 12.97 14.15 2,011,508 1,843,547 1,134 33.12 36.1
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) Sulfuric Acid Mist (SAM) Sulfuric Acid Mist (lb/hr) = SO ₂ Emission Rate (lb/hr) Conversion to H ₂ SO ₄ (% by weight) SAM Emission Rate (lb/hr) Lead Lead (lb/hr) = Basis (lb/10 12 Btu) x Heat Input (MM.	m) x 16 (mole. wgt CH ₄) x 211: NA 1 6.65 12.64 13.54 2,963,172 2,766,121 1,040 2.59 3.1 c) x Conversion to H ₂ SO ₄ (% b 3.4 10 0.34 Btu/hr) / 1,000,000 MMBtu/10 ¹²	NA 1 8.38 12.35 13.48 3.029,221 2,775,372 1,067 2.60 3.1 by weight)/100 3.3 10 0.33	NA 1 10.00 12.03 13.37 2,888,125 2,599,313 1,086 2,45 2,9	NA 20 5.49 13.59 14.38 2.086.449 1,971,903 1,066 35.88 39.0	NA 20 6.85 13.25 14.22 2,071,671 1,929,762 1,112 34.59 37.9	20 8.35 12.97 14.15 2,011,508 1,843,547 1,134 33.12 36.1
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) Sulfuric Acid Mist (SAM) Sulfuric Acid Mist (lb/hr)= SO ₂ Emission Rate (lb/hr) Conversion to H ₂ SO ₄ (% by weight) SAM Emission Rate (lb/hr) Lead Lead (lb/hr) = Basis (lb/10 12 Btu) x Heat Input (MM.) Heat Input (MMBtu/hr, HHV)	m) x 16 (mole. wgt CH_4) x 211: NA 1 6.65 12.64 13.54 2,963,172 2,766,121 1,040 2.59 3.1 c) x Conversion to H_2 SO $_4$ (% b 3.4 10 0.34 Btu/hr) /1,000,000 MMBtu/10 12 2,216	NA 1 8.38 12.35 13.48 3.029,221 2,775,372 1,067 2.60 3.1 by weight)/100 3.3 10 0.33	NA 1 10.00 12.03 13.37 2.888,125 2.599,313 1,086 2.45 2.9 3.1 10 0.31	NA 20 5.49 13.59 14.38 2.086,449 1,971,903 1,066 35.88 39.0	NA 20 6.85 13.25 14.22 2,071,671 1,929,762 1,112 34.59 37.9 2.0 10 0.20	20 8.35 12.97 14.15 2,011,508 1,843,547 1,134 33.12 36.1 1.9 10 0.19
VOC (lb/hr) = VOC (ppm actual) x Volume flow (acfi Basis, ppm actual Basis, ppm actual Basis, ppmvd @ 15% O ₂ Moisture (%) Oxygen (%) wet Oxygen (%) dry Flow (acfm) Flow (acfm), dry Exhaust Temperature (°F) VOC Emission Rate (lb/hr) Sulfuric Acid Mist (SAM) Sulfuric Acid Mist (lb/hr) = SO ₂ Emission Rate (lb/hr) Conversion to H ₂ SO ₄ (% by weight) SAM Emission Rate (lb/hr) Lead Lead (lb/hr) = Basis (lb/10 12 Btu) x Heat Input (MM.	m) x 16 (mole. wgt CH ₄) x 211: NA 1 6.65 12.64 13.54 2,963,172 2,766,121 1,040 2.59 3.1 c) x Conversion to H ₂ SO ₄ (% b 3.4 10 0.34 Btu/hr) / 1,000,000 MMBtu/10 ¹²	NA 1 8.38 12.35 13.48 3.029,221 2,775,372 1,067 2.60 3.1 by weight)/100 3.3 10 0.33	NA 1 10.00 12.03 13.37 2,888,125 2,599,313 1,086 2,45 2,9	NA 20 5.49 13.59 14.38 2.086.449 1,971,903 1,066 35.88 39.0	NA 20 6.85 13.25 14.22 2,071,671 1,929,762 1,112 34.59 37.9	20 8.35 12.97 14.15 2,011,508 1,843,547 1,134 33.12 36.1

Note: ppmvd= parts per million, volume dry; O₂= oxygen.

Source: Siemens, 2013



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Table S-B-5: Regulated and Hazardous Air Pollutant Emission Factors and Emissions for the Combustion Turbine Firing Gas and ULSD Oil Siemens F5

		Combus	tion Turbine	e		Combust	ion Turbin	е	<i>_</i>	Annual Emissions	: (TPY) "		
		Natu	ral Gas ^a			ULS	D Oil ^a		Scenario 1	Scenario 2	Maxin	num	
		Emission		Emission Rate		Emission		Emission Rate					
Pollutant	Reference	Factor	Units	(lb/hr)	Reference	Factor	Units	(lb/hr)	CT NG	CT NG & FO	1 CT	5 CT	
1,3-Butadiene	b,c	4.30E-07	lb/MMBtu	9.88E-04	f,c	1.60E-05	Ib/MMBtu	3.51E-02	1.67E-03	1.02E-02	1.02E-02	5.10E-0	
Acetaldehyde	b	4.00E-05	lb/MMBtu	9.19E-02				0.00E+00	1.56E-01	1.33E-01	1.56E-01	7.79E-0	
Acrolein	b	6.40E-06	lb/MMBtu	1.47E-02				0.00E+00	2.49E-02	2.12E-02	2.49E-02	1.25E-0	
Benzene	b	1.20E-05	lb/MMBtu	2.76E-02	f	5.50E-05	lb/MMBtu	1.21E-01	4.67E-02	7.00E-02	7.00E-02	3.50E-0	
	b						ID/WIIVIBLU		1.25E-01	1.06E-01	1.25E-01	6.23E-0	
Ethylbenzene	d	3.20E-05	lb/MMBtu	7.35E-02	d			0.00E+00					
Formaldehyde	b	2.06E-04	lb/MMBtu	4.73E-01	f	2.22E-04	lb/MMBtu	4.88E-01	8.01E-01	8.05E-01	8.05E-01	4.02E+	
Naphthalene Polycyclic Aromatic		1.30E-06	ib/MMBtu	2.99E-03	-	3.50E-05	lb/MMBtu	7.68E-02	5.06E-03	2.35E-02	2.35E-02	1.18E-0	
Hydrocarbons (PAH)	b,e	2.20E-06	lb/MMBtu	5.05E-03	f,e	4.00E-05	Ib/MMBtu	8.77E-02	8.57E-03	2.92E-02	2.92E-02	1.46E-0	
Propylene Oxide	b,c	2.90E-05	lb/MMBtu	6.66E-02				0.00E+00	1.13E-01	9.63E-02	1.13E-01	5.65E-0	
Toluene	b	3.30E-05	lb/MMBtu	7.58E-02				0.00E+00	1.28E-01	1.10E-01	1.28E-01	6.42E-0	
Xylene	b	6.40E-05	lb/MMBtu	1.47E-01				0.00E+00	2.49E-01	2.12E-01	2.49E-01	1.25E+(
2-Methylnaphthalene				0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
3-Methylchloranthrene				0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
7,12-Dimethylbenz(a)anthracene				0.00E+00		_		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+	
Acenaphthene				0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
Acenaphthylene				0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+	
Anthracene				0.00E+00		-		0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+	
Benz(a)anthracene				0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+	
Benzo(a)pyrene				0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
Benzo(b)fluoranthene				0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
Benzo(g,h,i)perylene				0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
Benzo(k)fluoranthene				0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
Chrysene				0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
Dibenzo(a,h)anthracene				0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
Dichlorobenzene				0.00E+00				0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+0	
Fluoranthene Fluorene				0.00E+00				0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+00 0.00E+00	0.00E+0	
Hexane ·				0.00E+00 0.00E+00				0.00E+00 0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
Indeno(1,2,3-cd)pyrene				0.00E+00				0.00E+00 0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
Phenanathrene				0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
Pyrene				0.00E+00				0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
Arsenic				0.00E+00	g,c	1.10E-05	lb/MMBtu	2.41E-02	0.00E+00	6.03E-03	6.03E-03	3.02E-0	
Beryllium				0.00E+00	g,c	3.10E-03	Ib/MMBtu	6.80E-04	0.00E+00	1.70E-04	1.70E-04	8.50E-0	
					9								
Cadmium				0.00E+00	9	4.80E-06	lb/MMBtu	1.05E-02	0.00E+00	2.63E-03	2.63E-03	1.32E-0	
Chromium				0.00E+00	¥	1.10E-05	lb/MMBtu	2.41E-02	0.00E+00	6.03E-03	6.03E-03	3.02E-0	
Cobalt				0.00E+00	0			0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+0	
Lead				0.00E+00	g	1.40E-05	lb/MMBtu	3.07E-02	0.00E+00	7.68E-03	7.68E-03	3.84E-0	
Manganese				0.00E+00	9	7.90E-04	lb/MMBtu	1.73E+00	0.00E+00	4.33E-01	4.33E-01	2.17E+0	
Mercury				0.00E+00	g	1.20E-06	lb/MMBtu	2.63E-03	0.00E+00	6.58E-04	6.58E-04	3.29E-	
Nickel				0.00E+00	g,c	4.60E-06	ib/MMBtu	1.01E-02	0.00E+00	2.52E-03	2.52E-03	1.26E-	
Selenium				0.00E+00	g,c	2.50E-05	Ib/MMBtu	5.48E-02	0.00E+00	1.37E-02	1.37E-02	6.85E-	
			Total HAPs =	0.98					1.66	1.62	1.73	8.67	
			idual HAP =						0.80	0.80	0.80	4.02	

^a Emissions based on:

Fuel Natural gas ULSD oil Heat input (MMBtu/hr) (HHV) (Base load at 75 °F) 2,297 2,193

Fuel	iel Scenario 1				
Natural Gas	3,390	2,89			
ULSD Oil	0	500			
Total Hours	3,390	3,39			



b Emission factor from Table 3.1-3, AP-42, EPA, April 2000. For Toluene, based on EPA database.

^c Based on the method detection limit; for the CT, based on 1/2 of the method detection limit; expected emissions are lower.

^d Formaldehyde emission factor based on 91 ppb @15% O₂ equivalent to combustion turbine MACT limit (see Table GE-A-6)

^e Assumed to be representative of Polycyclic Organic Matter (POM) emissions, a regulated HAP.

f Emission factor from Table 3.1-4, AP-42, EPA, April 2000.

⁹ Emission factor from Table 3.1-5, AP-42, EPA, April 2000.

h Annual operating hours



Table S-B-6: Maximum Formaldehyde Emissions when Firing Natural Gas and ULSD Oil Siemens F5

			CT at B	aseload			
		atural Gas-Firii ne Inlet Tempe			ULSD Oil-Firing Turbine Inlet Temper		
Parameter	35°F	75°F	95°F	35° F	75° F	95° F	
Formaldehyde (CH ₂ O)							
CH 2 O (lb/hr) = CH 2 O (ppm actual) x Vol	ume flow (acfm) x 30) (mole. wat CH	₂ O) x 2116.8 lb/ft	² (pressure) /			
L V / L WP			stant, R) x Actual	**	min/hr		
CH_2O (ppm actual) = CH_2O (ppmd @ 1	-		•				
Oxygen (%, dry)(O_2 dry) = Oxygen (%)/[,		, ,			
Basis, ppm actual- calculated	0.108	0.103	0.103	0.106	0.105	0.105	
CT, ppmvd @15% O ₂	0.091	0.091	0.091	0.091	0.091	0.091	
Moisture (%)	8.23	9.20	10.67	6.65	8.38	10.00	
Oxygen (%)	12.19	12.28	12.01	12.64	12.35	12.03	
Oxygen (%) dry	13.28	13.52	13.44	13.54	13.48	13.37	
Exhaust Flow (acfm)	2,882,874	3,091,716	2,942,724	2,963,172	3,029,221	2,888,125	
Exhaust Temperature (°F)	1,107	1,108	1,127	1,040	1,067	1,086	
Molecular weight	28.42	28.30	28.13	28.77	28.58	28.40	
CT Emission rate (lb/hr)	0.462	0.473	0.439	0.494	0.488	0.455	
Heat Input (MMBtu/hr, HHV)	2,246	2,297	2,147	2,216	2,193	2,059	
CT Emission rate (lb/10 ¹² Btu) (HHV)	205.8	205.8	204.7	222.9	222.3	221.0	
CT Emission rate (lb/10 ⁶ Btu) (HHV)	2.06E-04	2.06E-04	2.05E-04	2.23E-04	2.22E-04	2.21E-04	

Note: ppmvd= parts per million, volume dry; O₂= oxygen.

Source: Siemens, 2013 (CT Performance Data); Golder, 2013



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Table S-B-7: Hazardous Air Pollutant Emissions for Additional Emission Units - ULSD Oil-Firing Siemens F5

Parameter	Units	Value	Annual Emission Basis Black Start Diesel Engines
Number			4
Heat Input Rate	MMBtu/hr	per unit	47
Maximum operation/yr	hours	per unit	100
Heat Input Rate/annual	MMBtu/yr	all units	18,931
HAPs [Section 112(b) of Clean Air Act]	Emissio	n Factor ^{a, b}	Emissions (TPY)
Acrolein	lb/MMBtu	7.88E-06	7.46E-05
Acetaldehyde	lb/MMBtu	2.52E-05	2.39E-04
Benzene	lb/MMBtu	7.76E-04	7.35E-03
Formaldehyde	lb/MMBtu	7.89E-05	7.47E-04
Naphthalene	lb/MMBtu	1.30E-04	1.23E-03
Toluene	lb/MMBtu	2.81E-04	2.66E-03
Xylene	lb/MMBtu	1.93E-04	1.83E-03
Acenaphthene	lb/MMBtu	4.68E-06	4.43E-05
Acenaphthylene	lb/MMBtu	9.23E-06	8.74E-05
Anthracene	lb/MMBtu	1.23E-06	1.16E-05
Benzo(a)anthracene	lb/MMBtu	6.22E-07	5.89E-06
Benzo(b)fluoranthene	lb/MMBtu	1.11E-06	1.05E-05
Benzo(k)fluoranthene	lb/MMBtu	2.18E-07	2.06E-06
Benzo(g,h,i)perylene	lb/MMBtu	5.56E-07	5.26E-06
Benzo(a)pyrene	lb/MMBtu	2.57E-07	2.43E-06
Chrysene	lb/MMBtu	1.53E-06	1.45E-05
Dibenzo(a,h)anthracene	lb/MMBtu	3.46E-07	3.28E-06
Fluoanthene	lb/MMBtu	4.03E-06	3.81E-05
Fluorene	lb/MMBtu	4.47E-06	4.23E-05
Indo(1,2,3-cd)pyrene	lb/MMBtu	4.14E-07	3.92E-06
Phenanthrene	lb/MMBtu	1.05E-06	9.94E-06
Pyrene	lb/MMBtu	3.71E-06	3.51E-05
Arsenic	lb/10 ¹² Btu	4.0	3.79E-05
Beryllium	lb/10 ¹² Btu	3.0	2.84E-05
Cadmium	lb/10 ¹² Btu	3.0	2.84E-05
Chromium	lb/10 ¹² Btu	3.0	2.84E-05
Lead	lb/10 ¹² Btu	9.0	8 52F-05
	lb/10 Btu	3.0	2.84E-05
Mercury			
Manganese	lb/10 ¹² Btu	6.0	5.68E-05
Nickel	lb/10 ¹² Btu	3.0	2.84E-05
Selenium	lb/10 ¹² Btu	15.0	1.42E-04
Total HAPs =	=		1.49E-02
Max. Individual HAP			7.35E-03

^a EPA AP-42, Section 3.4, Large Stationary Diesel And All Stationary Dual-fuel Engines (October 1996)



^b EPA AP-42, Section 1.3, Fuel Oil Combustion for metals (September 1998).



Table S-B-8: Greenhouse Gas (GHG) Emissions Siemens F5

	Maxir Heat Inpu (MMB	t at 75°F	Emission (ib/MM		Hourly GHG (lb/l			ng Hours	Annual GHG		CO₂e Emis			CO₂e Emission Rate b (TPY)	
Pollutant	Natural Gas	ULSD Oil	Natural Gas	ULSD Oil	Natural Gas	ULSD Oil	Natural Gas	ULSD Oil	Natural Gas	ULSD Oil	Natural Gas	ULSD Oil	Natural Gas	ULSD Oil	Total
Natural Gas Or	ıly														
CO ₂	2,297	0.0	116.9	163.0	268,418.4	0.0	3,390	0	454,969.2	0	268,418.4	0.0	454,969.2	0	454,969.2
CH₄	2,297	0.0	0.002204	0.006612	5.1	0.0	3,390	0	8.6	0	106.3	0.0	180.2	0	180.2
N ₂ O	2,297	0.0	0.0002204	0.001322	0.5	0.0	3,390	0	0,9	0	156.9	0.0	266.0	0	266.0
										Total	268,681.7	0.0	455,415.4	0.0	455,415.4
Natural Gas &	Distillate Fuel Oil														
CO ₂	2,297	2,193.0	116.9	163.0	268,418.4	357,476.2	2,890	500	387,864.6	89,369.0	268,418.4	357,476.2	387,864.6	89,369.0	477,233.
CH₄	2,297	2,193.0	0.002204	0.006612	5.0626	14.5001	2,890	500	7.3	3.6	106.3	304.5	153.62	76.13	229.7
N ₂ O	2,297	2,193.0	0.0002204	0.001322	0.5063	2.9000	2,890	500	0.7	0.7	156.9	899.0	226.78	225	451.5
										Total	268,681.7	358,679.7	388,245.0	89,669.9	477,914
									Ma	aximum Total			455,415.4	89,669.9	477,914

^a Table C-2, Subpart C, 40 CFR 98. Emission factors in kg/MMBtu

Pollutant	Natural Gas	Distillate Fuel Oil
CO ₂	53.02	73.96
CH₄	0.001	0.003
N ₂ O	0.0001	0.0006

Conversion factor from kg/MMBtu to lb/MMBtu:

2.204

b CH₄ and N₂O are multiplied by CO₂e factor

Pollutant	CO _{2e} Factor
CH₄	21
N ₂ O	310



Table S-B-9: Greenhouse Gas (GHG) Emissions for Additional Emission Units Siemens F5

Emission Unit/ Pollutant	Maximum Heat Input (MMBtu/hr)			_	ons Rate (TPY) ^b er of Units		
Black Start Diesel En	gine (No. Units)					1	4
CO2	47	163.0	7,714.9	100	385.7	385.7	1,543.0
.CH₄	47	0.006612	0.313	100	0.016	0.33	1.3
N ₂ O	47	0.001322	0.063	100	0.0031	0.97	3.9
					-	387.0	1,548.2
Fire Pump Engine							
CO ₂	2.37	163.0	386.0	100	19.3	19.30	
CH₄	2.37	0.0	0.016	100	0.001	0.02	
N ₂ O	2.37	0.0	0.003	100	0.0002	0.05	
					-	19.4	-

^a Table C-2, Subpart C, 40 CFR 98. Emission factors in kg/MMBtu

Pollutant	Natural Gas	Distillate Fuel Oil
CO2	53.02	73.96
CH₄	0.001	0.003
N ₂ O	0.0001	0.0006

Conversion factor from kg/MMBtu to lb/MMBtu:

2.204

 $^{^{\}rm b}$ $~{\rm CH_4}$ and ${\rm N_2O}$ are multiplied by ${\rm CO_2e}$ factor

Pollutant	CO_{2e}	Factor
CH₄		21
N₂O	:	310



APPENDIX C

HISTORICAL ACTUAL EMISSION FROM EXISTING GT UNITS 1 THROUGH 24



Table 1: PFL GTs Nos. 1-12 and 13-24 Annual Heat Inputs, 2008 - 2012

	Heat Input fro	om Distillate Oi	l (MMBtu/yr)	Heat Inp	out from Natura (MMBtu/yr)	al Gas	Total	Actual Heat (MMBtu/yr)	nput	rating Hours /yr)	
Year	GTs # 1-12	GTs # 13-24	Total	GTs # 1-12	GTs # 13-24	Total	GTs # 1-12	GTs # 13-24	Total	GTs #1-12	GTs # 13-24
2012	305	1,292	1,597	318,000	341,000	659,000	318,305	342,292	660,597	1,146	1,317
2011	8,591	42,888	51,480	437,000	365,000	802,000	445,591	407,888	853,480	1,032	923
2010	210,800	320,280	531,080	677,000	310,000	987,000	887,800	630,280	1,518,080	2,003	1,341
2009	45,832	54,808	100,640	548,000	157,000	705,000	593,832	211,808	805,640	1,363	534
2008	13,052	14,828	27,880	316,950	137,600	454,550	330,002	152,428	482,430	741	357

Individual Fuel Heat Input as a Percent of Total Heat Input

	Heat Input fro	om Distillate Oil	Heat Input from Natural Gas (MMBtu/yr)						
Year	GTs #1-12	GTs # 13-24	Total	GTs # 1-12	GTs # 13-24	Total			
2012	0.0%	0.2%	0.2%	48.1%	51.6%	99.8%			
2011	1.0%	5.0%	6.0%	51.2%	42.8%	94.0%			
2010	13.9%	21.1%	35.0%	44.6%	20.4%	65.0%			
2009	5.7%	6.8%	12.5%	68.0%	19.5%	87.5%			
2008	2.7%	3.1%	5.8%	65.7%	28.5%	94.2%			

Note: All values are based on annual operating reports for the period 2008 - 2012.



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Table 2: Annual Emissions Reported in 2008-2012 Annual Operating Reports

Year	Pollutant	CTs # 1-12 (tons)	CTs #13-24 (tons)	Total (tons)
2012	NO _x	113.6	120.4	234.0
	co	65.9	78.0	143.9
	SO ₂	0.2	0.2	0.4
	voc	0.2	0.3	0.6
	РМ	1.1	1.1	2.2
	PM ₁₀	1.1	1.1	2.2
	SAM ^a	0.0	0.0	0.1
	CO ₂			
2011	NO _x	108.1	102.9	211.0
	co	24.3	16.0	40.3
	SO ₂	. 23.9	29.9	53.8
	VOC	0.4	0.4	0.8
	PM	1.5	1.5	3.0
	PM ₁₀	1.5	1.5	3.0
	SAM ^a	2.9	3.7	8.2
	CO₂	_		
2010	NO _x	223.6	181.7	405.3
	co	42.4	24.9	67.2
	SO₂	38.0	57.5	95.6
	VOC	1.3	0.7	2.0
	PM	3.6	3.0	6.6
	PM ₁₀	3.6	3.0	6.6
	SAM ^a	4.7	7.0	14.6
	CO ₂			
2009	NO _x	68.1	32.1	100.2
	co	31.3	10.0	41.2
	SO₂	8.7	8.1	16.8
	voc	1.0	0.3	1.3
	PM	2.1	0.9	3.0
	PM ₁₀	2.1	0.9	3.0
	SAM ^a	1.1	1.0	2.6
	CO ₂	-		
2008	NO _x	7 4 .4	35.5	109.9
	co	17.8	7.9	25.7
	SO₂	2.4	2.7	5.1
	VOC	0.5	0.2	0.8
	PM	1.1	0.6	1.7
	PM ₁₀	1.1	0.6	1.7
	SAM ^a	0.3	0.3	0.8
	CO ₂			

Source: Annual Operating Report (AOR) for PFL, 2008 - 2012.

^a Not reported in AORs - based on assuming 10% of SO₂ converts to SO₃, all of which converts to SAM.





Table 3: Actual Emissions as a Function of Heat Input, 2008 - 2012

GTs # 1-12

	Actual Annual Heat Input			GTs#	1-12 Acti	ual Emis	sions (TP	Y) ^b		Emissions per Unit Heat Input ^c (Ib/MMBtu)							
Year	(MMBtu/yr) ^a	NOx	со	voc	SO ₂	PM	PM ₁₀	SAM d	CO₂ e	NO _x	со	voc	SO ₂	PM	PM ₁₀	SAM ^d	CO2 e
2012	318,305	113.6	65.9	0.2	0.2	1,1	1.1	0.0		0.7138	0.4140	0.0014	0.0013	0.0066	0.0066	0.0002	
2011	445,591	108.1	24.3	0.4	23.9	1.5	1.5	3.7		0.4852	0.1088	0.0020	0.1073	0.0067	0.0067	0.0164	
2010	887,800	223.6	42.4	1.3	38.0	3.6	3.6	5.8		0.5038	0.0955	0.0029	0.0856	0.0081	0.0081	0.0131	
2009	593,832	68.1	31.3	1.0	8.7	2.1	2.1	1.3		0.2294	0.1053	0.0032	0.0293	0.0072	0.0072	0.0045	
2008	330,002	74.4	17.8	0.5	2.4	1.1	1.1	0.4		0.4506	0.1076	0.0033	0.0147	0.0070	0.0070	0.0023	
									Maximum =	0.7138	0.4140	0.0033	0.1073	0.0081	0.0081	0.0164	

GTs # 13-24

	Actual Annual Heat Input			GTs#1	13-24 Act	ual Emis	sions (TF	PY) ^b				Emis	sions per (lb/M	Unit Heat I MBtu)	Input ^c		
Year	(MMBtu/yr) ^a	NO _x	со	voc	SO ₂	PM	PM ₁₀	SAM d	CO₂°	NO _x	со	voc	SO ₂	PM	PM ₁₀	SAM ^d	CO₂°
2012	342,292	120.4	78.0	0.3	0.2	1.1	1.1	0.0	**	0.7035	0.4555	0.0020	0.0010	0.0066	0.0066	0.0002	
2011	407,888	102.9	16.0	0.4	29.9	1.5	1.5	4.6		0.5045	0.0787	0.0018	0.1466	0.0073	0.0073	0.0224	
2010	630,280	181.7	24.9	0.7	57.5	3.0	3.0	8.8		0.5766	0.0789	0.0023	0.1826	0.0097	0.0097	0.0280	
2009	211,808	32.1	10.0	0.3	8.1	0.9	0.9	1.2		0.3031	0.0942	0.0029	0.0765	0.0082	0.0082	0.0117	
2008	152,428	35.5	7.9	0.2	2.7	0.6	0.6	0.4		0.4661	0.1040	0.0032	0.0354	0.0073	0.0073	0.0054	
									Maximum =	0.7035	0.4555	0.0032	0.1826	0.0097	0.0097	0.0280	

GTs # 1-12 and 13-24

	Actual Annual Heat Input		GTs #	£ 1-12 and	1 13-24 To	otal Actu	ıal Emiss	ions (TPY)	b	Emissions per Unit Heat Input ^c (Ib/MMBtu)							
Year	(MMBtu/yr) ^a	NO _x	со	voc	SO ₂	PM	PM ₁₀	SAM ^d	CO₂ e	NOx	со	voc	SO ₂	PM	PM ₁₀	SAM ^d	CO2
2012	660,597	234.0	143.9	0.6	0.4	2.2	2.2	0.1		0.7085	0.4355	0.0017	0.0011	0.0066	0.0066	0.0002	
2011	853,480	211.0	40.3	8.0	53.8	3.0	3.0	8.2		0.4944	0.0944	0.0019	0.1261	0.0070	0.0070	0.0193	
2010	1,518,080	405.3	67.2	2.0	95.6	6.6	6.6	14.6		0.5340	0.0886	0.0027	0.1259	0.0087	0.0087	0.0193	
2009	805,640	100.2	41.2	1.3	16.8	3.0	3.0	2.6		0.2487	0.1023	0.0031	0.0417	0.0075	0.0075	0.0064	
2008	482,430	109.9	25.7	8.0	5.1	1.7	1.7	8.0		0.4555	0.1065	0.0033	0.0213	0.0071	0.0071	0.0033	
	·								Maximum =	0.7085	0.4355	0.0033	0.1261	0.0087	0.0087	0.0193	

^a Based on AOR data; see Table 1.



^b Based on AOR data; see Table 2.

^c Total actual emissions divided by total heat input.

^d Not reported in AORs - based on assuming 10% of SO₂ converts to SO₃, all of which converts to SAM.

^e See Table 4 for CO₂ calculation.



Table 4: Estimated Actual Annual Emissions of $\mathrm{N_2O}$, $\mathrm{CH_{4,}CO_2}$ for the Period 2008 - 2012

PFL GTs Nos. 1-12 and 13-24

	Actual		N₂O Er	nissions			CH₄ En	nissions		CO ₂ Emissions			
	Annual	Emission			CO₂e °	Emission			CO₂e °	Emission			
	Heat Input ^a	Factor ^b	Annual	Emissions	Rate	Factor ^b	Annual	Emissions	Rate	Factor ^d	Annual Em	issions	
Unit	(MMBtu/yr)	(lb/MMBtu)	(lb/yr)	(TPY)	(TPY)	(lb/MMBtu)	(lb/yr)	(TPY)	(TPY)	(lb/MMBtu)	(lb/yr)	(TPY)	
Distillate Oil													
2012	1,597	1.32E-03	2.1	1.06E-03	0.3	6.6E-03	10.6	5.28E-03	0.1	1.6E+02	260,356	130	
2011	51,480	1.32E-03	68.1	3.40E-02	10.6	6.6E-03	340.4	1.70E-01	3.6	1.6E+02	8,391,584	4,196	
2010	531,080	1.32E-03	702.3	3.51E-01	108.9	6.6E-03	3,511.5	1.76E+00	36.9	1.6E+02	86,570,204	43,28	
2009	100,640	1.32E-03	133.1	6.65E-02	20.6	6.6E-03	665.4	3.33E-01	7.0	1.6E+02	16,405,109	8,20	
2008	27,880	1.32E-03	36.9	1.84E-02	5.7	6.6E-03	184.3	9.22E-02	1.9	1.6E+02	4,544,659	2,27	
latural Gas-l	- -iring												
2012	659,000	2.20E-04	145.2	0.073	22.5	2.2E-03	1,452.4	0.726	15.3	1.2E+02	77,008,157	38,50	
2011	802,000	2.20E-04	176.8	0.088	27.4	2.2E-03	1,767.6	0.884	18.6	1.2E+02	93,718,576	46,85	
2010	987,000	2.20E-04	217.5	0.109	33.7	2.2E-03	2,175.3	1.088	22.8	1.2E+02	115,336,951	57,66	
2009	705,000	2.20E-04	155.4	0.078	24.1	2.2E-03	1,553.8	0.777	16.3	1.2E+02	82,383,536	41,19	
2008	454,550	2.20E-04	100.2	0.050	15.5	2.2E-03	1,001.8	0.501	10.5	1.2E+02	53,116,931	26,55	
otal													
2012	660,597		147	0.1	22.8		1,463	0.7	15.4		77,268,513	38,63	
2011	853,480		245	0.1	37.9		2,108	1.1	22.1		102,110,160	51,0	
2010	1,518,080		920	0.5	142.6		5,687	2.8	59.7		201,907,155	100,9	
2009	805,640		288	0.1	44.7		2,219	1.1	23.3		98,788,645	49,39	
2008	482,430		137	0.1	21.2		1,186	0.6	12.5		57,661,590	28,8	

^a Based on AOR data; see Table 1.



^b Table C-2, Subpart C, 40 CFR 98. Emission factors in kg/MMBtu were converted to lb/MMBtu by multiplying by 2.204.

^c N₂O and CH₄ are multiplied by a factor of 310 and 21, respectively, to determine CO ₂ equivalence.

^d Table C-1, Subpart C, 40 CFR 98. Emission factors in kg/MMBtu were converted to lb/MMBtu by multiplying by 2.204.



Table 5: Annual Average Emissions for GTs #1-12 and 13-24 for Each Consecutive Two-Year Period, 2008-2012

	An	nual Emission	ons for GTs #	1-12 and 13-	-24		Maximum 2-year			
_	2012	2011	2010	2009	2008	2012-2011	2011-2010	2010-2009	2009-2008	Average (tons/yr)
Pollutant						(tons)	(tons)	(tons)	(tons)	
NO _x	234.0	211.0	405.3	100.2	109.9	222.5	308.2	252.8	105.0	308.2
CO	143.9	40.3	67.2	41.2	25.7	92.1	53.8	54.2	33.5	92.1
SO₂	0.4	53.8	95.6	16.8	5.1	27.1	74.7	56.2	11.0	74.7
VOC	0.6	0.8	2.0	1.3	0.8	0.7	1.4	1.6	1.0	1.6
PM	2.2	3.0	6.6	3.0	1.7	2.6	4.8	4.8	2.4	4.8
PM ₁₀	2.2	3.0	6.6	3.0	1.7	2.6	4.8	4.8	2.4	4.8
PM _{2.5} a	2.2	3.0	6.6	3.0	1.7	2.6	4.8	4.8	2.4	4.8
SAM ^b	0.1	8.2	14.6	2.6	0.8	4.1	11. 4	8.6	1.7	11.4
CHG ^c (CO₂e)	38,672	51,115	101,156	49,462	28,864	44,894	76,136	75,309	39,163	76,135.5

^a Assuming equal to PM₁₀ emissions.

Source: Annual Operating Report (AOR) for 2008 - 2012; EPA's Acid Rain database.



 $^{^{\}rm b}$ Not reported in AORs - based on assuming 10% of SO $_{\rm 2}$ converts to SO $_{\rm 3}$, all of which converts to SAM.

^c Calculated based on actual annual heat input - see Table 4.

APPENDIX D BACT DETERMINATIONS FOR SIMPLE CYCLE CTS

Table D-1: Summary of NO_x BACT Determinations for Natural Gas-Fired CTs (2003-2013)

Facility Name	State	Permit Issued	Process Info	Heat Input	Control Method	NO _x Limit	Basis
<u>ilorida</u>							
EA Greenland Energy Center	FL	3/10/2009 Turbine, Simple	Cycle, Natural Gas	190 MW	DLN and WI	9 PPMVD @ 15% O2	BACT-PSD
Shady Hills Generating Station	FL	1/12/2009 Two Simple Cy	cle Combustion Turbine - Model 7FA	170 MW	DLN	9 PPMVD @ 15% O2	BACT-PSD
Progress Bartow Power Plant	FL	1/26/2007 Simple Cycle C	ombustion Turbine (1)	1972 MMBTU/H	DLN and WI	15 PPMVD	BACT-PSD
EA- St. Johns River Park Plant	FL	12/22/2006 Simple Cycle T	, ,	1804 MMBTU/H	DLN and Wi	15 PPM @ 15% O2	OTHER CASE-BY-CAS
Dleander Power Project	FL	11/17/2006 Simple Cycle C		190 MW	DLN and WI	9 PPM @15% O2	BACT-PSD
EC/Polk Power Energy Station	FL	4/28/2006 Simple Cycle G		1834 MMBTU/H	DLN	9 PPMVD @ 15% O2	BACT-PSD
PL Martin Plant	FL	4/16/2003 Turbine, Simple		170 MW	DLN	9 PPMVD @ 15% O2	BACT-PSD
PA Region 4 (AL, FL, GA, KY, MS, NC, SC, TN)							
Dahlberg Combusdtion Turbine Electric Generating Facility	GA	5/14/2010 Simple Cycle C	ombustion Turbine - Electric Generating Plant	1530 MW	DLN And Wi	9 PPM @ 15% O2	BACT-PSD
exxon Mobile Bay Northwest Gulf Field	AL	2/1/2005 Turbine, Simple	: Cyde	6000 BHP	Solonox Combustor	25 PPM @ 15% O2	BACT-PSD
exxon Mobile Mobile Bay - Bon Secure Bay Field	AL	2/1/2005 Turbine, Simple	e Cycle	3600 BHP	Solonox Combustion	25 PPM @ 15% O2	BACT-PSD
VA - Kemper Combustion Turbine Plant	MS	12/10/2004 GE Combustion	Turbine (4)	1278 MMBTU/H		12 PPM @ 15% O2	BACT-PSD
Moselle Plant	MS	12/10/2004 Combustion Tu	rbine, Gas-Fired, Simple-Cycle	1143.3 MMBTU/H	DLN Burner With Inlet Gas Cooling.	9 PPM VD @ 15% O2	BACT-PSD
ouisville Gas And Electric Company	KY	6/6/2003 Turbine, Simple	: Cycle, Natural Gas (6)	160 MW	DLN Combustors	12 PPM @ 15% O2	BACT-PSD
Smepa - Silver Creek Generating	MS	5/29/2003 Turbine, Simple	Cycle (3)	1109.3 MMBTU/H	DLN Burners	9 PPM @ 15% O2	BACT-PSD
Other States							
IRG Marsh Landing	CA	· •	Cycle, Natural Gas (4)	190 MW	DLN and hot SCR	2.5 PPMVD @15% O2	BACT-PSD
R.M. Heskett Station	ND	2/22/2013 Combustion Tu	-	986 MMBTU/H	DLN	9 PPMVD @15% O2	BACT-PSD
Sosque County Power Plant	TX	2/27/2009 Electrical Gene		170 MW	DLN	9 PPMVD @15% O2	BACT-PSD
Great River Energy - Elk River Station	MN	7/1/2008 Combustion Tu		2169 MMBTU/H	DLN	9 PPM	BACT-PSD
Rawhide Energy Station	CO	8/31/2007 Unit F Combust		1400 MMBTU/H	DLN	9 PPMVD	BACT-PSD
Ve Energies Concord	WI		rbine, 100 Mw, Natural Gas	100 MW	WI	25 PPMDV @ 15% O2	BACT-PSD
airbault Energy Park	MN	7/15/2004 Turbine, Simple	• ,	1663 MMBTU/H	DLN In Lean Premix Mode.	25 PPMVD @ 15% 02	BACT-PSD
Great River Energy Lakefield Junction Station	MN	9/10/2003 Turbine, Simple		109 MW	DLN and GCP	9 PPM @ 15% O2	BACT-PSD
DDEC - Louisa Facility	VA	3/11/2003 Turbine, Simple	• • • • • • • • • • • • • • • • • • • •	1624 MMBTU/H	GCP And CEM System.	10.5 PPMVD @ 15% O2	N/A
DDEC - Marsh Run Facility DDEC -Marsh	VA VA	2/14/2003 Turbine, Simple 2/14/2003 Turbine, Simple	•	1624 MMBTU/H	DLN Burners DLN and WI	9 PPMVD @ 15% O2 10.5 PPMVD	N/A BACT-PSD

Source: EPA 2013 (RBLC database); Golder, 2013

Note: DLN= dry low NOx; WI= water injection; SI=Steam Injection; GCP= good combustion practices; SCR= selective catalytic reduction



Table D-2: Summary of NO_x BACT Determinations for ULSD Oil-Fired CTs (2003-2013)

Facility Name	State	Permit Issued Process Info	Heat Input	Fuel	Control Method	NO _x Limit	Basis
<u>Florida</u>							
JEA Greenland Energy Center	FL	3/10/2009 Turbine, Simple Cycle, Natural Gas	190 MW	NO.2 FUEL OIL	WI	42 PPMVD @ 15% O2	BACT-PSD
Shady Hills Generating Station	FL	1/12/2009 Two Simple Cycle Combustion Turbine - Model 7FA	170 MW	NO.2 FUEL OIL	WI	42 PPMVD @ 15% O2	BACT-PSD
FPL MARTIN PLANT	FL	12/22/2003 TURBINE, SIMPLE CYCLE, FUEL OIL (4)	170 MW	NO.2 FUEL OIL	WI	42 PPMVD @ 15% O2	BACT-PSD
EPA Region 4 (AL, FL, GA, KY, MS, NC, SC, TN)					ı		
TVA - KEMPER COMBUSTION TURBINE PLANT	MS	1/25/2005 GENERAL ELECTRIC COMBUSTION TURBINES		NO.2 FUEL OIL	WI	42 PPMDV @ 15% O2	BACT-PSD
Talbot Energy Facility	GA	6/9/2003 Turbine, Simple Cycle, Fuel Oil, (2)	108 MW	NO.2 FUEL OIL	DLN and WI	42 PPMDV @ 15% O2	BACT-PSD
Broad River Energy Center	SC	5/22/2003 Combustion Turbines		NO.2 FUEL OIL	WI	42 PPMDV @ 15% O2	BACT-PSD
Other States							
WE ENERGIES CONCORD	WI	11/29/2006 COMBUSTION TURBINE, 100 MW, #2 FUEL OIL	100 MW	No. 2 FUEL OIL	WI	65 PPMDV @ 15% O2	BACT-PSD
FAIRBAULT ENERGY PARK	MN	9/21/2004 TURBINE, SIMPLE CYCLE, DISTILLATE OIL (1)	1576 MMBTU/H	No. 2 FUEL OIL	WI	42 PPMDV @ 15% O2	BACT-PSD
ODEC - LOUISA	VA	6/21/2004 TURBINE, SIMPLE CYCLE, FUEL OIL (1)	1820 MMBTU/H	No. 2 FUEL OIL	WI	42 PPMVD @ 15% O2	BACT-PSD
ODEC - LOUISA FACILITY	VA	4/28/2003 TURBINE, SIMPLE CYCLE, (1), FUEL OIL	1820 MMBTU/H	No. 2 FUEL OIL	GCP AND CEM SYSTEM.	42 PPMVD @ 15% O2	BACT-PSD
Great River Energy Lakefield Junction Station	MN	9/10/2003 Turbine, Simple Cycle, Fuel Oil	109 MW	No. 2 FUEL OIL	WI and GCP	42 PPMVD @ 15% O2	BACT-PSD
ODEC - Marsh Run Facility	VA	2/14/2003 Turbine, Simple Cycle, (4), Fuel Oil	1803 MMBTU/H	No. 2 FUEL OIL	DLN BURNERS, CLEAN BURNING FUEL, AND CEM SYSTEM.	62 PPMVD @ 15% O2	NA

Source: EPA 2013 (RBLC database); Golder, 2013

Note: SCR= selective catalytic reduction; WI= water injection; GCP= good combustion practices



Table D-3: Summary of CO BACT Determinations for Natural Gas-Fired CTs (2003-2013)

Facility Name	State	Permit Issued	Process Info	Heat Input	Control Method	CO Limit	Basis
Florida							
JEA Greenland Energy Center	FL	3/10/2009 TURBINE, SIM	PLE CYCLE, NATURAL GAS	190 MW	GCP	4.1 PPMVD @ 15% O2	BACT-PSD
SHADY HILLS GENERATING STATION	FL	1/12/2009 TWO SIMPLE (CYCLE COMBUSTION TURBINE - MODEL 7FA	170 MW	GCP	6.5 PPMVD @ 15% O2	Avoid PSD
JEA Kennedy7 Generating Station	FL	12/4/2008 TURBINE, SIM	PLE CYCLE, NATURAL GAS	172 MW	GCP	9 PPMVD @ 15% O2	BACT-PSD
Orlando Utilities- Curtis H Station Energy Center	FL	5/12/2008 TURBINE, SIM	PLE CYCLE, NATURAL GAS	170 MW	GCP	8 PPMVD @ 15% O2	BACT-PSD
Oleander Power Project	FL	11/17/2006 Simple Cycle C	ombustion Turbine	190 MW	GCP	9 PPM @15% O2	OTHER CASE-BY-CASE
TEC/Polk Power Energy Station	FL	4/28/2006 Simple Cycle G	as Turbine	1834 MMBTU/H	GCP '	9 PPMVD @ 15% O2	Avoid PSD
FPL MARTIN PLANT	FL	4/16/2003 TURBINE, SIM	PLE CYCLE, NATURAL GAS, (4)	170 MW	GCP	8 PPMVD @ 15% O2	BACT-PSD
EPA Region 4 (AL, FL, GA, KY, MS, NC, SC, TN)							
DAHLBERG COMBUSDTION TURBINE ELECTRIC GENERATING FACILITY	GA	5/14/2010 SIMPLE CYCL	E COMBUSTION TURBINE - ELECTRIC GENERATING PLANT	1530 MW	GCP	9 PPM @ 15% O2	BACT-PSD
TVA - KEMPER COMBUSTION TURBINE PLANT	MS	12/10/2004 GENERAL ELE	CTRIC COMBUSTION TURBINES			20 PPM @ 15% 02	BACT-PSD
TVA - KEMPER COMBUSTION TURBINE PLANT	MS	12/10/2004 EMISSION PO	NT (4)	1278 MMBTU/H		25 PPM @ 15% 02	BACT-PSD
MOSELLE PLANT	MS	12/10/2004 COMBUSTION	TURBINE, GAS-FIRED, SIMPLE-CYCLE	1143.3 MMBTU/H		20 PPM @ 15% 02	BACT-PSD
LOUISVILLE GAS AND ELECTRIC COMPANY	KY	6/6/2003 TURBINE, SIM	PLE CYCLE, NATURAL GAS (6)	160 MW	GCP	9 PPM @ 15% 02	BACT-PSD
SMEPA - SILVER CREEK GENERATING	MS	5/29/2003 TURBINE, SIM	PLE CYCLE (3)	1109.3 MMBTU/H	GCP	25 PPM @ 15% 02	BACT-PSD
Other States							
R.M. HESKETT STATION	ND	2/22/2013 Combustion Tu	rbine	986 MMBtu/hr	GCP	25 PPMVD@15% O2	BACT-PSD
PSEG FOSSIL LLC KEARNY GENERATING STATION	NJ	10/27/2010 SIMPLE CYCLI	TURBINE	8940000 MMBtu/year (HHV)	Oxidation Catalyst, GCP	5 PPMVD@15% O2	OTHER CASE-BY-CASE
HOWARD DOWN STATION	NJ	9/16/2010 SIMPLE CYCLI	E (NO WASTE HEAT RECOVERY)(>25 MW)	5000 MMFT3/YR	THE TURBINE WILL UTILIZE A CATALYTIC	5 PPMVD@15%O2	OTHER CASE-BY-CASE
BAYONNE ENERGY CENTER	NJ	9/24/2009 COMBUSTION	TURBINES, SIMPLE CYCLE, ROLLS ROYCE, 8	603 MMBTU/H	CO OXIDATION CATALYST AND CLEAN E	5 PPMVD@15%O2	OTHER CASE-BY-CASE
FAIRBAULT ENERGY PARK	MN	7/15/2004 TURBINE, SIM	PLE CYCLE, NATURAL GAS (1)	1663 MMBTU/H	GCP.	10 PPMVD @ 15% O2	BACT-PSD
ODEC - LOUISA FACILITY	VA	3/11/2003 TURBINE, SIM	PLE CYCLE, (4), NATURAL GAS	901 MMBTU/H	GCP AND A CONTINUOUS EMISSION MO	25 PPMVD @ 15% O2	N/A
ODEC - LOUISA FACILITY	VA	3/11/2003 TURBINE, SIM	PLE CYCLE, (1), NATURAL GAS	1624 MMBTU/H	GCP AND CONTINUOUS EMISSION MON	9 PPMVD @ 15% O2	N/A

Source: EPA 2013 (RBLC database); Golder, 2013

Note: DB = duct burner; GCP= good combustion practices



Table D-4: Summary of CO BACT Determinations for ULSD Oil-Fired CTs (2003-2013)

Facility Name	State	Permit Issued	Process Info	Heat Input	Fuel	Control Method	CO Limit	Basis
<u>Georqia</u>								
JEA Greenland Energy Center	FL	3/10/2009 Turbine	, Simple Cycle, Natural Gas	NO.2 FUEL OIL	170 MW	GCP	8 PPMVD @ 15% O2	BACT-PSD
Shady Hills Generating Station	FL	1/12/2009 Two Sir	mple Cycle Combustion Turbine - Model 7FA	NO.2 FUEL OIL	170 MW	GCP	13.5 PPMVD @ 15% O2	BACT-PSD
FPL MARTIN PLANT	FL	4/16/2003 TURBIN	NE, SIMPLE CYCLE, FUEL OIL (4)	NO.2 FUEL OIL	170 MW	GCP	15 PPMVD @ 15% O2	BACT-PSD
PA Region 4 (AL, FL, GA, KY, MS, NC, SC, TN)								
TVA - KEMPER COMBUSTION TURBINE PLANT	MS	1/25/2005 GENER	AL ELECTRIC COMBUSTION TURBINES	NO.2 FUEL OIL			20 PPM @ 15% O2	BACT-PSD
BROAD RIVER ENERGY CENTER	SC	12/17/2012 COMBL	JSTION TURBINES	NO.2 FUEL OIL		GCP AND CLEAN BURNING FUELS	20 PPMVD @ 15% O2	BACT-PSD
Other States								
FAIRBAULT ENERGY PARK	MN	7/15/2004 TURBIN	NE, SIMPLE CYCLE, DISTILLATE OIL (1)	NO.2 FUEL OIL	1576 MMBTU/I	H GCP.	10 PPMVD @ 15% O2	BACT-PSD
FAIRBAULT ENERGY PARK	MN	7/15/2004 TURBIN	NE, COMBINED CYCLE, DISTILLATE OIL (1)	NO.2 FUEL OIL	1801 MMBTU/I	H GCP.	10 PPMVD @ 15% O2	BACT-PSD
DDEC - LOUISA FACILITY	VA	3/11/2003 TURBIN	NE, SIMPLE CYCLE, (1), FUEL OIL	NO.2 FUEL OIL	1820 MMBTU/I	GCP AND CEM SYSTEM.	20 PPMVD @ 15% O2	N/A
SP Nelson Energy, LLC	IL	1/28/2000 CT, CC	w/ Duct Burner	NO.2 FUEL OIL	2166 MMBtu/hi	GCP and Combustion Controls	0.1024 lb/MMBtu	

Source: EPA 2013 (RBLC database); Golder, 2013

Note: GCP= good combustion practices



Table D-5: Summary of VOC BACT Determinations for Natural Gas-Fired CTs (2003-2013)

		Permit					
Facility Name	State	Issued Process Info	Fuel	Heat Input	Control Method	VOC Limit	Basis
0							
Georgia Progress Bartow Power Plant	FL	1/26/2007 Simple Cycle Combustion Turbine (1)	NATURAL GAS	1972 MMBTU/H	GCP	1.2 PPMVD	BACT-PSD
FPL Martin Plant	-	4/16/2003 Turbine, Simple Cycle, Natural Gas, (4)	NATURAL GAS	170 MW	GCP		
FFL Warun Flant	FL	4/16/2003 Turbine, Simple Cycle, Natural Gas, (4)	NATURAL GAS	170 10100	GCF	1.3 PPMVD @ 15% O2	BACT-PSU
EPA Region 4 (AL, FL, GA, KY, MS, NC, SC, TN)							
Dahlberg Combusdtion Turbine Electric Generating	Fac GA	5/14/2010 Simple Cycle Combustion Turbine - Electric Generating Plant	NATURAL GAS	1530 MW	GCP	5 PPM@15%02	BACT-PSD
TVA - Kemper Combustion Turbine Plant	MS	12/10/2004 GE Cornbustion Turbine (4)	NATURAL GAS	1278 MMBTU/H		70 LB/H	
Talbot Energy Facility	GA	6/9/2003 Turbine, Simple Cycle, Natural Gas, (6)	NATURAL GAS	108 MW	GCP	0.0086 LB/MMBTU	BACT-PSD
Rincon Power Plant	GA	3/24/2003 Combustion Turbine, (2)	NATURAL GAS	171.7 MW	Oxidation Catalyst	2 PPM @ 15% O2	BACT-PSD
Other States							
Calcasieu Plant	LA	12/21/2011 Turbine Exhaust Stack No. 1 & No. 2	NATURAL GAS	1900 MM BTU/H EAG	CH DLN Combustors	7 LB/H	BACT-PSD
Pseg Fossil Llc Kearny Generating Station	NJ	10/27/2010 Simple Cycle Turbine	Natural Gas	8940000 MMBtu/year (H	HV, Oxidation Catalyst and CGP	4 PPMVD@15% O2	OTHER CASE-BY-CASE
Bosque County Power Plant	TX	2/27/2009 Electrical Generation	NATURAL GAS	170 MW	BACT IS THE USE OF GCP TO MINIMIZE THE F	4 PPMVD	BACT-PSD
CPV St Charles	MD	11/12/2008 Combustion Turbines (2)	NATURAL GAS		OXIDATION CATALYST	1 PPMVD @ 15% O2	LAER
NRG Texas Electric Power Generation	TX	4/19/2006 Annual Limits	NATURAL GAS AND FUEL OIL			38.8 T/YR	BACT-PSD
Dayton Power And Light Company	ОН	3/7/2006 Combustion Turbines (2), Simple Cycle	NATURAL GAS	1115 MMBTU/H		10 LB/H	OTHER CASE-BY-CASE
Rolling Hills Generating Plant	ОН	1/17/2006 Natural Gas Fired Turbines (5)	NATURAL GAS	209 MW		3.2 LB/H	BAT (Non-US ONLY)
Rohm And Haas Chemicals Llc Lone Star Plant	TX	3/24/2005 L-Area Gas Turbine	NATURAL GAS			0.59 LB/H	RACT
Jack County Power Plant	TX	7/22/2003 Combustion Turbine With 550 Mmbtu/Hr Duct Burner	NATURAL GAS		GCP	20.6 LB/H	BACT-PSD
Exxon Mobil Chemical Baytown Olefins Plant	TX	6/13/2003 164 Mw Gas Turbine-Case 1	NATURAL GAS			3.17 LB/H	BACT-PSD
Union Carbide Texas City Operations	TX	1/23/2003 Turbine Only	NATURAL GAS	12000 LB/H		0.16 LB/H	BACT-PSD
Chickahominy Power	VA	1/10/2003 Turbine, Simple Cycle, Natural Gas, (4)	NATURAL GAS	182.6 MW	CLEAN FUEL, GCP	3.7 LB/H	BACT-PSD

Source: EPA 2013 (RBLC database); Golder, 2013

Note: DLN= dry low NOx; GCP= good combustion practices.



Table D-6: Summary of VOC BACT Determinations for ULSD Oil-Fired CTs (2003-2013)

Facility Name	State	Permit Issued	Process Info	Heat Input	Fuel	Control Method	VOC Limit	Basis
Florida FPL Martin Plant	FL	4/16/2003 Turbine S	Simple Cycle, Fuel Oil (4)	170 MW	NO.2 FUEL OIL	GCP	2.5 PPMVD @ 15% O2	BACT-PSD
	1 L	4/ 10/2003 14/5/10, 0	milple cycle, r doi on (1)	170 14144	140.21 022 012	001	2.3 11 1414 5 6 1370 32	BA01-1 0B
EPA Region 4 (AL, FL, GA, KY, MS, NC, S	C, TN)							
Talbot Energy Facility	GA	6/9/2003 Turbine, S	imple Cycle, Fuel Oil, (2)	108 MW	NO.2 FUEL OIL		0.0149 LB/MMBTU	BACT-PSD
TVA - Kemper Combustion Turbine Plant	MS	12/10/2004 GE Comb	ustion Turbine (4)	1278 MMBTU/H	NO.2 FUEL OIL		70 LB/R	BACT-PSD
Other States								
Dayton Power & Light Energy Llc	ОН	12/3/2009 Turbines (4), Simple Cycle, Fuel Oil #2	4216 H/YR	NO.2 FUEL OIL		5.5 LB/H	BACT-PSD
CPV St Charles	MD	11/12/2008 Internal Co	ombustion Engine - Emergency Gene	rator	NO.2 FUEL OIL		4.8 G/HP-H	BACT-PSD
						Use Of Low-Sulfur Fuels, Limiting		
Arsenal Hill Power Plant	LA	3/20/2008 Dfp Diese	l Fire Pump	310 HORSEPOWER	NO.2 FUEL OIL	Operating Hours And Proper Engine Maintenance	0.77 LB/H	BACT-PSD
Creole Trail Lng Import Terminal	LA	8/15/2007 Submerge	d Combustion Vaporizer Nos. 1-21	108 MMBTU/H EA.	NO.2 FUEL OIL	GCP	0.32 LB/H	BACT-PSD
Dayton Power And Light Company	ОН	3/7/2006 Combustic	on Turbines (2), Simple Cycle	1115 MMBTU/H	NO.2 FUEL OIL		10 LB/H	OTHER CASE-BY-CASE
Dayton Power And Light Company	ОН	3/7/2006 Combustic	on Turbine (1), Simple Cycle	1115 MMBTU/H	NO.2 FUEL OIL		10 LB/H	OTHER CASE-BY-CASE
Chickahominy Power	VA	1/10/2003 Turbine, S	imple Cycle, Fuel Oil, (4)	182.6 MW	NO.2 FUEL OIL	Clean fuel, GCP	27.6 LB/H	BACT-PSD

Source: EPA 2013 (RBLC database); Golder, 2013

Note: DLN= dry low NOx; GCP= good combustion practices.



Table D-7: Summary of GHG (CO2e) BACT Determinations for Natural Gas-Fired CTs (2003-2013)

Facility Name	State	Permit Issued	Process Info	Heat Input	Control Method	CO₂e Limit	Basis
PIO PICO ENERGY CENTER R.M. HESKETT STATION SABINE PASS LNG TERMINAL	CA ND LA	5/8/2013 Combusti	STION TURBINES (NORMAL OPERATION) ion Turbine ycle Generation Turbines (2)	300 MW 986 MMBtu/hr 286 MMBTU/H	GCP and fueled by natural gas - use GE LM2500+G4 turbines	1,328 LB/MW-HR 413,198 TONS 4,872,107 TONS/YR	BACT-PSD BACT-PSD BACT-PSD

Source: EPA 2013 (RBLC database); Golder, 2013

Note: GCP= good combustion practices



Table D-8: Summary of PM BACT Determinations for Natural Gas-Fired CTs (2003-2013)

								PM/PM ₁₀ /PM _{2.5}	
Facility Name	State	Permit Issued	Process Info	Heat Input	pollutant	Control Method	PM/PM ₁₀ /PM _{2.5} Limit	Emissions Rate	Basis
ilorida									
Shady Hills Generating Station	FL	1/12/2009 Two Simp	le Cycle Combustion Turbine - Model 7fa	170 MW	PM10		10 % OPACITY		BACT-PSD
Jacksonville Electric Authority/Jea	FL	12/22/2006 Simple Cy	cle Turbine 172 Mw	1804 MMBTU/H	filterable PM10	Clean Fuel			BACT-PSD
Dleander Power Project	FL		cle Combustion Turbine	190 MW	filterable PM10	Clean Fuel	1.5 GR S/100 SCF		BACT-PSD
FEC/Polk Power Energy Station	FL	4/28/2006 Simple Cy		1834 MMBTU/H	filterable PM10	Clean Fuel, GCP	10 % OPACITY		BACT-PSD
FPL Martin Plant FPL Manatee Plant - Unit 3	FL FL		Simple Cycle, Natural Gas, (4) Simple Cycle, Natural Gas, (4)	170 MW 170 MW	filterable PM10 filterable PM10	Clean Fuel Clean Fuel			BACT-PSD BACT-PSD
EPA Region 4 (AL, FL, GA, KY, MS, NC, SC,	TN)								
Dahlberg Combusdtion Turbine Electric		Simple Cu	cle Combustion Turbine						
Generating Facility	GA	5/14/2010	cie Combustion Turbine	1530 MW	PM10	Clean Fuel, GCP		0.011 LB/MMBTU	BACT-PSD
TVA - Kemper Combustion Turbine Plant	MS	12/10/2004 GE Comb	ustion Turbine (4)	1278 MMBTU/H	PM			0.0084 LB/MMBTU	OTHER CASE-BY-CAS
Moselle Plant	MS	12/10/2004 Combustic	on Turbine, Gas-Fired, Simple-Cycle	1143.3 MMBTU/H	filterable PM10			10 LB/H	BACT-PSD
Talbot Energy Facility	GA	6/9/2003 Turbine, S	imple Cycle, Natural Gas, (6)	108 MW	PM	Clean Fuel		7.35 LB/H	BACT-PSD
ouisville Gas And Electric Company	KY	6/6/2003 Turbine, S	simple Cycle, Natural Gas (6)	160 MW	PM	GCP		7.35 LB/H	BACT-PSD
SMEPA - Silver Creek Generating	MS	5/29/2003 Turbine, S	•	1109.3 MMBTU/H	filterable PM10	Clean Fuel, GCP		7.35 LB/H	BACT-PSD
Rincon Power Plant	GA	3/24/2003 Combustic		171.7 MW	PM	Clean Fuel		7.35 LB/H	BACT-PSD
Varren Peaking Power Facility (Warren Power,			Simple Cycle, Natural Gas (4)	959.8 MMBTU/H	PM	Clean Fuel		7 LB/H	BACT-PSD
Varren Peaking Power Facility (Warren Power,			Simple Cycle, Natural Gas (4)	959.8 MMBTU/H	filterable PM10	Clean Fuel		7 LB/H	BACT-PSD
Other States									
R.M. Heskett Station	ND	2/22/2013 Combustic	on Turbine	986 MMBtu/hr	PM10	GCP		7.3 LB/HR	BACT-PSD
Pio Pico Energy Center	CA	11/19/2012 Combustic	on Turbines (Normal Operation)	300 MW	PM10	Clean Fuel		0.0065 LB/MMBTU (HIBACT-PSD
Great River Energy - Elk River Station	MN	7/1/2008 Combustic	on Turbine Generator	2169 MMBTU/H	PM10	Clean Fuel			BACT-PSD
Great River Energy - Elk River Station	MN	7/1/2008 Combustic	on Turbine Generator	2169 MMBTU/H	filterable PM10	Clean Fuel			BACT-PSD
Great River Energy - Elk River Station	MN	7/1/2008 Combustic	on Turbine Generator	2169 MMBTU/H	filterable PM10	Clean Fuel			BACT-PSD
Vestern Farmers Electric Anadarko	OK	6/13/2008 Combustic	on Turbine Peaking Unit(S)	462.7 MMBTU/H	filterable PM10			4 LB/H	BACT-PSD
Rawhide Energy Station	СО	8/31/2007 Unit F Cor	mbustion Turbine	1400 MMBTU/H	PM	Clean Fuel		18 LB/H	BACT-PSD
Rawhide Energy Station	СО	8/31/2007 Unit F Cor	mbustion Turbine	1400 MMBTU/H	filterable PM10	Clean Fuel		18 LB/H	BACT-PSD
Dayton Power And Light Company	ОН	3/7/2006 Combustic	on Turbine (1), Simple Cycle	1115 MMBTU/H	filterable PM10			8 LB/H	OTHER CASE-BY-CAS
Dayton Power And Light Company	ОН	3/7/2006 Combustic	on Turbines (2), Simple Cycle	1115 MMBTU/H	filterable PM10			8 LB/H	OTHER CASE-BY-CAS
Ve Energies Concord	WI	1/26/2006 Combustic	on Turbine, 100 Mw, Natural Gas	100 MW	РM			39 LB/H	BACT-PSD
Rolling Hills Generating Plant	ОН	1/17/2006 Natural Ga	as Fired Turbines (5)	209 MW	PM			17.3 LB/H	BAT (Non-US ONLY)
Rolling Hills Generating Plant	ОН	1/17/2006 Natural Ga		209 MW	filterable PM10			17.3 LB/H	BACT-PSD
South Harper Peaking Facility	MO		Simple Cycle, Natural Gas, (3)	1455 MMBTU/H	filterable PM10	GCP		15.25 LB/H	
airbault Energy Park	MN		imple Cycle, Natural Gas (1)	1663 MMBTU/H	filterable PM10	Clean Fuel, GCP		0.01 LB/MMBTU	BACT-PSD
Fredonia Energy Station	WA	7/18/2003 Turbines, \$		108 MW	filterable PM10	Clean Fuel, GCP	0.01 GR/DSCF		BACT-PSD
Exxon Mobil Chemical Baytown Olefins Plant	TX	6/13/2003 Gas Turbir		164 MW	PM	3 4-1, 4		18 LB/H	BACT-PSD
DDEC - Louisa Facility	VA		imple Cycle, (1), Natural Gas	1624 MMBTU/H	filterable PM10	GCP		18 LB/H	N/A
DDEC - Louisa	VA		imple Cycle, Natural Gas (1)	1624 MMBTU/H	filterable PM10	Clean Fuel, GCP		18 LB/H	BACT-PSD
DDEC -Marsh	VA		imple Cycle, Natural Gas, (4)	1624 MMBTU/H	filterable PM10	Clean Fuel, GCP		18 LB/H	BACT-PSD
Chickahominy Power	VA	1/10/2003 Turbine, S		182.6 MW	filterable PM10	Clean Fuel, GCP		27 LB/H	BACT-PSD



Table D-9: Summary of PM BACT Determinations for ULSD Oil-Fired CTs (2000-2013)

				-					PM/PM ₁₀ /PM _{2.5}	
Facility Name	State	Permit Issued	Process Info	Heat Input	Fuel	Pollutant	Control Method	PM/PM ₁₀ /PM _{2.5} Limit	Emissions Rate	Basis
-										_
Florida FPL Martin Plant	FL	4/46/2002 Turki	as Simple Cycle Evel Oil (4)	170 MW	NO.2 FUEL OIL	filterable PM10	Clean Fuel			BACT-PSD
Greenland Energy Center	FL	3/10/2009 Comb	ne, Simple Cycle, Fuel Oil (4)	190 MW	NO.2 FUEL OIL	PM10	Clean Fuel	10% OPACITY		BACT-PSD
orcemand Energy Schief	1.	3/10/2003 COM	Justion Turbine	130 11114	110.21 022 012	1 10110	Oldan Faci	10/0 01/10/11		<i>5</i> /101105
EPA Region 4 (AL, FL, GA, KY, MS, NC, SC	TN)									
Talbot Energy Facility	GA	6/9/2003 Turbi	ne, Simple Cycle, Fuel Oil, (2)	108 MW	NO.2 FUEL OIL	PM	Clean Fuel		0.023 LB/MMBT	UBACT-PSD
TVA - Kemper Combustion Turbine Plant	MS	12/10/2004 GE C	combustion Turbine (4)	1278 MMBTU/H	NO.2 FUEL OIL	filterable PM10	Clean Fuel		15.8 LB/H	BACT-PSD
Broad River Energy Center	SC	5/22/2003 Comb	oustion Turbines		NO.2 FUEL OIL	PM	Clean Fuel		46 LB/H	BACT-PSD
Other States										
Dayton Power And Light Company	ОН	3/7/2006 Comb	oustion Turbines (2), Simple Cycle	1115 MMBTU/H	NO.2 FUEL OIL	filterable PM10	Clean Fuel		15 LB/H	OTHER CASE-BY-CASE
Dayton Power And Light Company	ОН	3/7/2006 Comb	oustion Turbine (1), Simple Cycle	1115 MMBTU/H	NO.2 FUEL OIL	filterable PM10	Clean Fuel		15 LB/H	OTHER CASE-BY-CASE
Fairbault Energy Park	MN	7/15/2004 Turbi	ne, Simple Cycle, Distillate Oil (1)	1576 MMBTU/H	NO.2 FUEL OIL	PM	Clean Fuel		0.03 LB/MMBT	U BACT-PSD
ODEC - Louisa Facility	VA	3/11/2003 Turbit	ne, Simple Cycle, (1), Fuel Oil	1820 MMBTU/H	NO.2 FUEL OIL	filterable PM10	Clean Fuel		36 LB/H	N/A
ODEC - Louisa	VA	3/11/2003 Turbii	ne, Simple Cycle, Fuel Oil (1)	1820 MMBTU/H	NO.2 FUEL OIL	filterable PM10	Clean Fuel		36 LB/H	BACT-PSD
ODEC - Marsh Run Facility	VA	2/14/2003 Turbit	ne, Simple Cycle, (4), Fuel Oil	1803 MMBTU/H	NO.2 FUEL OIL	filterable PM10	Clean Fuel		36 LB/H	N/A
Chickahominy Power	VA	1/10/2003 Turbi	ne, Simple Cycle, Fuel Oil, (4)	182.6 MW	NO.2 FUEL OIL	filterable PM10	Clean Fuel		27 LB/H	BACT-PSD

Source: EPA 2013 (RBLC database); Golder, 2013

Note: GCP= good combustion practices



APPENDIX E

FDEP FORM NO. 62-210.900(1)
APPLICATION FOR AIR PERMIT – LONG FORM



Department of Environmental Protection RECEIVED

Division of Air Resource Management

APPLICATION FOR AIR PERMIT - LONG FORM

JUL 3 1 2013

I. APPLICATION INFORMATION

DIVISION OF AIR RESOURCE MANAGEMENT

Air Construction Permit – Use this form to apply for an air construction permit:

- For any required purpose at a facility operating under a federally enforceable state air operation permit (FESOP) or Title V air operation permit;
- For a proposed project subject to prevention of significant deterioration (PSD) review, nonattainment new source review, or maximum achievable control technology (MACT);
- To assume a restriction on the potential emissions of one or more pollutants to escape a requirement such as PSD review, nonattainment new source review, MACT, or Title V; or
- To establish, revise, or renew a plantwide applicability limit (PAL).

Air Operation Permit – Use this form to apply for:

- An initial federally enforceable state air operation permit (FESOP); or
- An initial, revised, or renewal Title V air operation permit.

To ensure accuracy, please see form instructions.

Identification of Facility

14	therine action of 1 active					
1.	Facility Owner/Company Name: Flo	rida Pov	wer & L	ight Compai	ny	
2.	Site Name: Lauderdale Plant					
3.	Facility Identification Number: 0110	037				
4.	Facility Location Street Address or Other Locator: 2 M	files We	st of Ra	venswood F	Road	
	City: Ft. Lauderdale Co	unty: B	roward		Zip Code: 33004	
5.	Relocatable Facility? ☐ Yes ☐ No			_	V Permitted Facility? ☐ No	
<u>Ap</u>	oplication Contact					
1.	Facility Contact Name: Matthew Raffenberg, Senior Director	of Envir	onment	al Licensing		
2.	Facility Contact Mailing Address Organization/Firm: Florida Power &	Light Co	ompany	,		
	Street Address: 700 Universe Box	ulevard	JES/JE			

Application Processing Information (DEP Use)

City: Juno Beach

3. Facility Contact Telephone Numbers:

Telephone: (561) 691-2808

1. Date of Receipt of Application: 7-31-13	3. PSD Number (if applicable):
2. Project Number(s): 0 1 00 3 1 - 011 - NO	4. Siting Number (if applicable):

ext.

State: FL

PSD-FL-423

4. Facility Contact E-mail Address: Matthew.Raffenberg@FPL.com

Zip Code: **33408**

Fax: (561) 691-7070

Purpose of Application

This application for air permit is being submitted to obtain: (Check one)
Air Construction Permit
 ☐ Air construction permit to establish, revise, or renew a plantwide applicability limit (PAL). ☐ Air construction permit to establish, revise, or renew a plantwide applicability limit (PAL), and separate air construction permit to authorize construction or modification of one or more emissions units covered by the PAL.
Air Operation Permit
☐ Initial Title V air operation permit.
☐ Title V air operation permit revision.
☐ Title V air operation permit renewal.
☐ Initial federally enforceable state air operation permit (FESOP) where professional engineer (PE) certification is required.
☐ Initial federally enforceable state air operation permit (FESOP) where professional engineer (PE) certification is not required.
Air Construction Permit and Revised/Renewal Title V Air Operation Permit (Concurrent Processing)
☐ Air construction permit and Title V permit revision, incorporating the proposed project.
☐ Air construction permit and Title V permit renewal, incorporating the proposed project.
Note: By checking one of the above two boxes, you, the applicant, are requesting concurrent processing pursuant to Rule 62-213.405, F.A.C. In such case, you must also check the following box:
☐ I hereby request that the department waive the processing time requirements of the air construction permit to accommodate the processing time frames of the Title V air operation permit.

Application Comment

This application is for the Site Certification Application (SCA) modification and environmental permitting associated with the replacement of gas turbines (GTs) at the FPL Fort Lauderdale Plant, and at the FPL Port Everglades Plant, Broward County, Florida. FPL plans to replace the existing 24 simple cycle GTs with a net capability of 1,004 megawatts (MW) with five simple cycle combustion turbines (CTs) that will be rated at approximately 200 MW each (Lauderdale CT Project). The new CTs will be designated as Units 6A through 6E.

Scope of Application

Emissions		Air	Air Permit
Unit ID	Description of Emissions Unit	Permit	Processing
Number	•	Type	Fee
Units 6A	Five Siemens SImple-Cycle Combustion	AC1A	
through	Turbines	ACTA	
6E	Turbines		
<u> </u>	-OR-		
	-OK-		
Units 6A	Five GE SImple-Cycle Combustion Turbines	AC1A	
through			
6E			
	-AND-		
2	Four Black-Start Diesel Engines	AC1A	
-	Tour Black Glart Blood Engines	AGIA	
3	Two Fuel Tanks	AC1A	
		1	
4 1' ' T	·		

Application Processing Fee	
Check one: Attached - Amount: \$ 7,500	☐ Not Applicable

\Box	Not	Ann	انمما	പിച

Owner/Authorized Representative Statement

Complete if applying for an air construction permit or an initial FESOP.

1. Owner/Authorized Representative Name:

Randall R. LaBauve, Vice President, Environmental Services

2. Owner/Authorized Representative Mailing Address...

Organization/Firm: Florida Power & Light Company Street Address: 700 Universe Boulevard, JES/JB

City: Juno Beach

State: FL

Zip Code: **33408**

3. Owner/Authorized Representative Telephone Numbers...

Telephone: (561) 691-7001

ext. Fax: (561) 691-7070

4. Owner/Authorized Representative E-mail Address: Randall.R.LaBauve@FPL.com

5. Owner/Authorized Representative Statement:

I, the undersigned, am the owner or authorized representative of the corporation, partnership, or other legal entity submitting this air permit application. To the best of my knowledge, the statements made in this application are true, accurate and complete, and any estimates of emissions reported in this application are based upon reasonable techniques for calculating emissions. I understand that a permit, if granted by the department, cannot be transferred without authorization from the department.

Signature

7/29/2013

Application Responsible Official Certification

Complete if applying for an initial, revised, or renewal Title V air operation permit or concurrent processing of an air construction permit and revised or renewal Title V air operation permit. If there are multiple responsible officials, the "application responsible official" need not be the "primary responsible official."

1. Application Responsible Official Name:		
2. Application Responsible Official Qualification (Check one or more of the following options, as applicable):		
For a corporation, the president, secretary, treasurer, or vice-president of the corporation in charge of a principal business function, or any other person who performs similar policy or decision-making functions for the corporation, or a duly authorized representative of such		
person if the representative is responsible for the overall operation of one or more manufacturing, production, or operating facilities applying for or subject to a permit under Chapter 62-213, F.A.C.		
 For a partnership or sole proprietorship, a general partner or the proprietor, respectively. For a municipality, county, state, federal, or other public agency, either a principal executive officer or ranking elected official. 		
☐ The designated representative at an Acid Rain source or CAIR source.		
3. Application Responsible Official Mailing Address Organization/Firm:		
Street Address:		
City: State: Zip Code:		
4. Application Responsible Official Telephone Numbers Telephone: () ext. Fax: ()		
Telephone: () ext. Fax: () 5. Application Responsible Official E-mail Address:		
6. Application Responsible Official Certification:		
I, the undersigned, am a responsible official of the Title V source addressed in this air permit application. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements made in this application are true, accurate and complete and that, to the best of my knowledge, any estimates of emissions reported in this application are based upon reasonable techniques for calculating emissions. The air pollutant emissions units and air pollution control equipment described in this application will be operated and maintained so as to comply with all applicable standards for control of air pollutant emissions found in the statutes of the State of Florida and rules of the Department of Environmental Protection and revisions thereof and all other applicable requirements identified in this application to which the Title V source is subject. I understand that a permit, if granted by the department, cannot be transferred without authorization from the department, and I will promptly notify the department upon sale or legal transfer of the facility or any permitted emissions unit. Finally, I certify that the facility and each emissions unit are in compliance with all applicable requirements to which they are subject, except as identified in compliance plan(s) submitted with this application.		
Signature Date		

Professional Engineer Certification

l.	Professional Engineer Name: Kennard F. Kosky
	Registration Number: 14996
2.	Professional Engineer Mailing Address
	Organization/Firm: Golder Associates Inc.**
	Street Address: 6026 NW 1st Place
	City: Gainesville State: FL Zip Code: 32607
3.	Professional Engineer Telephone Numbers
	Telephone: (352) 336-5600 ext. 21156 Fax: (352) 336-6603
4.	Professional Engineer E-mail Address: Ken_Kosky@golder.com
5.	Professional Engineer Statement:
	I, the undersigned, hereby certify, except as particularly noted herein*, that:
	(1) To the best of my knowledge, there is reasonable assurance that the air pollutant emissions unit(s) and the air pollution control equipment described in this application for air permit, when properly operated and maintained, will comply with all applicable standards for control of air pollutant emissions found in the Florida Statutes and rules of the Department of Environmental Protection; and
	(2) To the best of my knowledge, any emission estimates reported or relied on in this application are true, accurate, and complete and are either based upon reasonable techniques available for calculating emissions or, for emission estimates of hazardous air pollutants not regulated for an emissions unit addressed in this application, based solely upon the materials, information and calculations submitted with this application.
	(3) If the purpose of this application is to obtain a Title V air operation permit (check here \square , if so), I further certify that each emissions unit described in this application for air permit, when properly operated and maintained, will comply with the applicable requirements identified in this application to which the unit is subject, except those emissions units for which a compliance plan and schedule is submitted with this application.
	(4) If the purpose of this application is to obtain an air construction permit (check here \boxtimes , if so) or concurrently process and obtain an air construction permit and a Title V air operation permit revision or renewal for one or more proposed new or modified emissions units (check here \square , if so), I further certify that the engineering features of each such emissions unit described in this application have been designed or examined by me or individuals under my direct supervision and found to be in conformity with sound engineering principles applicable to the control of emissions of the air pollutants characterized in this application.
	(5) If the purpose of this application is to obtain an initial air operation permit or operation permit revision or renewal for one or more newly constructed or modified emissions units (check here , if so), I further certify that, with the exception of any changes detailed as part of this application, each such emissions unit has been constructed or modified in substantial accordance with the information given in the corresponding application for air construction permit and with all provisions contained in such permit. Total Total

* Attach any exception to certification statement.

**Board of Professional Engineers Certificate of Authorization #00001670.

DEP Form No. 62-210.900(1) Form Effective: 03/11/2010

II. FACILITY INFORMATION

A. GENERAL FACILITY INFORMATION

Facility Location and Type

1. Facility UTM Coordinates Zone 17 East (km) 580.2 North (km) 2883.3		2. Facility Latitude/Longitude Latitude (DD/MM/SS) 26/4/5 Longitude (DD/MM/SS) 80/11/54				
3.	Governmental Facility Code:	4. Facility Status Code:	5.	Facility Major Group SIC Code: 49	6.	Facility SIC(s): 4911
7.	Facility Comment :					

Facility Contact

1.	Facility Contact Name:		
	Dwayne Harper, Plant General Manage	er .	
2.	Facility Contact Mailing Address		
	Organization/Firm: FPL Lauderdale P	'lant	
	Street Address: 4300 SW 42nd Ave	enue	
	City: Fort Lauderdale	State: FL	Zip Code: 33314
3.	Facility Contact Telephone Numbers:		
	Telephone: (954) 797-1582 es	xt.	Fax: (954) 797-1579
4.	Facility Contact E-mail Address:	,	

Facility Primary Responsible Official

Complete if an "application responsible official" is identified in Section I that is not the facility "primary responsible official."

	• - • -					
1.	Facility Primary Responsible	Official Name:				
2.	Facility Primary Responsible Organization/Firm: Street Address:	Official Mailing	Address			
	City:	State:			Zip Code:	
3.	Facility Primary Responsible	Official Telephor	ne Numbers	•••		
	Telephone: ()	ext.	Fax:	()	
4.	Facility Primary Responsible	Official E-mail A	ddress:			

Facility Regulatory Classifications

Check all that would apply *following* completion of all projects and implementation of all other changes proposed in this application for air permit. Refer to instructions to distinguish between a "major source" and a "synthetic minor source."

1. ☐ Small Business Stationary Source ☐ Unknown
2. ☐ Synthetic Non-Title V Source
3. ⊠ Title V Source
4. Major Source of Air Pollutants, Other than Hazardous Air Pollutants (HAPs)
5. Synthetic Minor Source of Air Pollutants, Other than HAPs
6. Major Source of Hazardous Air Pollutants (HAPs)
7. Synthetic Minor Source of HAPs
8. One or More Emissions Units Subject to NSPS (40 CFR Part 60)
9. More Emissions Units Subject to Emission Guidelines (40 CFR Part 60)
10. ☑ One or More Emissions Units Subject to NESHAP (40 CFR Part 61 or Part 63)
11. Title V Source Solely by EPA Designation (40 CFR 70.3(a)(5))
12. Facility Regulatory Classifications Comment:
FPL Combustion Turbines are subject to NSPS 40 CFR 60 Subpart KKKK and 40 CFR 63 Subpart YYYY.
Subpart YYYY. The facility will have several reciprocating internal combustion engines (RICE) that are
Subpart YYYY. The facility will have several reciprocating internal combustion engines (RICE) that are
Subpart YYYY. The facility will have several reciprocating internal combustion engines (RICE) that are
Subpart YYYY. The facility will have several reciprocating internal combustion engines (RICE) that are
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Subpart YYYY. The facility will have several reciprocating internal combustion engines (RICE) that are

List of Pollutants Emitted by Facility

1. Pollutant Emitted	2. Pollutant Classification	3. Emissions Cap [Y or N]?
PM/PM10	A	N
NOx	A	N
СО	Α	N
VOC	A	N
SO2	A	N
Pb	Α	N
SAM	Α	N
HAPS	A	N
-		
 		
	·	

B. EMISSIONS CAPS

Facility-Wide or Multi-Unit Emissions Caps

. Pollutant	2. Facility-	3. Emissions	4. Hourly	5. Annual	6. Basis for
Subject to	Wide Cap	Unit ID's	Cap	Cap	Emissions
Emissions	[Y or N]?	Under Cap	(lb/hr)	(ton/yr)	Cap
Сар	(all units)	(if not all units)			
		_		<u> </u>	
. Facility-W	ide or Multi-Unit	Emissions Cap Con	nment:		
. Facility-W	ide or Multi-Unit	Emissions Cap Con	nment:		
. Facility-W	ide or Multi-Unit	Emissions Cap Con	nment:		
. Facility-W	ide or Multi-Unit	Emissions Cap Con	nment:		
. Facility-W	ide or Multi-Unit	Emissions Cap Con	nment:		
. Facility-W	ide or Multi-Unit	Emissions Cap Con	nment:		
. Facility-W	ide or Multi-Unit	Emissions Cap Con	nment:		
. Facility-W	ide or Multi-Unit	Emissions Cap Con	nment:		
. Facility-W	ide or Multi-Unit	Emissions Cap Con	nment:		
. Facility-W	ide or Multi-Unit	Emissions Cap Con	nment:		
. Facility-W	ide or Multi-Unit	Emissions Cap Con	nment:		

C. FACILITY ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1.	Facility Plot Plan: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) ☑ Attached, Document ID: See Air Report ☐ Previously Submitted, Date: ☐
2.	Process Flow Diagram(s): (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) ☑ Attached, Document ID: See Air Report ☐ Previously Submitted, Date:
3.	Precautions to Prevent Emissions of Unconfined Particulate Matter: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: See Air Report Previously Submitted, Date:
Ad	Iditional Requirements for Air Construction Permit Applications
	Area Map Showing Facility Location: ☐ Attached, Document ID: See Air Report ☐ Not Applicable Cisting permitted facility)
2.	Description of Proposed Construction, Modification, or Plantwide Applicability Limit (PAL): ☑ Attached, Document ID: See Air Report
3.	Rule Applicability Analysis: ☑ Attached, Document ID: See Air Report
4.	List of Exempt Emissions Units: ☐ Attached, Document ID: ☐ Not Applicable (no exempt units at facility)
5.	Fugitive Emissions Identification: ☐ Attached, Document ID: ☐ Not Applicable
6.	Air Quality Analysis (Rule 62-212.400(7), F.A.C.): ☑ Attached, Document ID: See Air Report □ Not Applicable
7.	Source Impact Analysis (Rule 62-212.400(5), F.A.C.):
8.	Air Quality Impact since 1977 (Rule 62-212.400(4)(e), F.A.C.):
9.	Additional Impact Analyses (Rules 62-212.400(8) and 62-212.500(4)(e), F.A.C.): ✓ Attached, Document ID: See Air Report ✓ Not Applicable
10.	. Alternative Analysis Requirement (Rule 62-212.500(4)(g), F.A.C.): ☐ Attached, Document ID: ☐ Not Applicable

C. FACILITY ADDITIONAL INFORMATION (CONTINUED)

Additional Requirements for FESOP Applications

1.	List of Exempt Emissions Units: ☐ Attached, Document ID: ☐ Not Applicable (no exempt units at facility)
Ac	Iditional Requirements for Title V Air Operation Permit Applications
1.	List of Insignificant Activities: (Required for initial/renewal applications only) Attached, Document ID: Not Applicable (revision application)
2.	Identification of Applicable Requirements: (Required for initial/renewal applications, and for revision applications if this information would be changed as a result of the revision being sought) Attached, Document ID:
	☐ Not Applicable (revision application with no change in applicable requirements)
3.	Compliance Report and Plan: (Required for all initial/revision/renewal applications) Attached, Document ID:
	Note: A compliance plan must be submitted for each emissions unit that is not in compliance with all applicable requirements at the time of application and/or at any time during application processing. The department must be notified of any changes in compliance status during application processing.
4.	List of Equipment/Activities Regulated under Title VI: (If applicable, required for initial/renewal applications only) Attached, Document ID:
	☐ Equipment/Activities Onsite but Not Required to be Individually Listed ☐ Not Applicable
5.	Verification of Risk Management Plan Submission to EPA: (If applicable, required for initial/renewal applications only) Attached, Document ID: Not Applicable
6.	Requested Changes to Current Title V Air Operation Permit: Attached, Document ID: Not Applicable

C. FACILITY ADDITIONAL INFORMATION (CONTINUED)

Additional Requirements for Facilities Subject to Acid Rain, CAIR, or Hg Budget Program

1.	Acid Rain Program Forms:
	Acid Rain Part Application (DEP Form No. 62-210.900(1)(a)):
	Phase II NO _X Averaging Plan (DEP Form No. 62-210.900(1)(a)1.): ☐ Attached, Document ID: ☐ Previously Submitted, Date: ☐ Not Applicable
	New Unit Exemption (DEP Form No. 62-210.900(1)(a)2.): ☐ Attached, Document ID: ☐ Previously Submitted, Date: ☐ Not Applicable
2.	CAIR Part (DEP Form No. 62-210.900(1)(b)): ☐ Attached, Document ID: FPL-AR-3 ☐ Not Applicable (not a CAIR source) ☐ Previously Submitted, Date:
	I Not Applicable (not a CARC source)
A	dditional Requirements Comment
Ac	<u> </u>
A	<u> </u>
Ac	<u> </u>

Section [1]

FPL - CT No. 6A through 6E

III. EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Application - For Title V air operation permitting only, emissions units are classified as regulated, unregulated, or insignificant. If this is an application for an initial, revised or renewal Title V air operation permit, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each regulated and unregulated emissions unit addressed in this application. Some of the subsections comprising the Emissions Unit Information Section of the form are optional for unregulated emissions units. Each such subsection is appropriately marked. Insignificant emissions units are required to be listed at Section II, Subsection C.

Air Construction Permit or FESOP Application - For air construction permitting or federally enforceable state air operation permitting, emissions units are classified as either subject to air permitting or exempt from air permitting. The concept of an "unregulated emissions unit" does not apply. If this is an application for an air construction permit or FESOP, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air permitting are required to be listed at Section II, Subsection C.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit Application – Where this application is used to apply for both an air construction permit and a revised or renewal Title V air operation permit, each emissions unit is classified as either subject to air permitting or exempt from air permitting for air construction permitting purposes, and as regulated, unregulated, or insignificant for Title V air operation permitting purposes. A separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit addressed in this application that is subject to air construction permitting and for each such emissions unit that is a regulated or unregulated unit for purposes of Title V permitting. (An emissions unit may be exempt from air construction permitting but still be classified as an unregulated unit for Title V purposes.) Emissions units classified as insignificant for Title V purposes are required to be listed at Section II, Subsection C.

If submitting the application form in hard copy, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application must be indicated in the space provided at the top of each page.

DEP Form No. 62-210.900(1) Effective: 03/11/2010

Section [1] FPL - CT No. 6A through 6E

A. GENERAL EMISSIONS UNIT INFORMATION

1. Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised

<u>Title V Air Operation Permit Emissions Unit Classification</u>

	or renewal Title V permit or FESOP		kip this item if applying	for an air construction
	☐ The emissions emissions unit		Emissions Unit Informati	ion Section is a regulated
	☐ The emissions unregulated en		missions Unit Informati	on Section is an
En	nissions Unit Desci	ription and Status		
1.	Type of Emissions	Unit Addressed in this	Section: (Check one)	
	single process	or production unit, or a	ion addresses, as a singl ctivity, which produces definable emission point	one or more air
	of process or p	roduction units and acti	· · · · · · · · · · · · · · · · · · ·	e emissions unit, a group one definable emission
				e emissions unit, one or fugitive emissions only.
2.		issions Unit Addressed cle CTs or Siemens Sim		
3.	Emissions Unit Ide	entification Number: U	nits 6A, 6B, 6C, 6D, and	6E
4.	Emissions Unit	5. Commence	6. Initial Startup	7. Emissions Unit
	Status Code:	Construction	Date:	Major Group
	A	Date: 2014	2016	SIC Code:
8.	Federal Program A	npplicability: (Check al	l that apply)	<u>.l</u>
	Acid Rain Unit	t		
	□ CAIR Unit			
9.	Package Unit: Manufacturer:		Model Number:	
10.	Generator Namepla	ate Rating: 200 MW/C	T	
11.	Emissions Unit Co	mment:		

DEP Form No. 62-210.900(1) Effective: 03/11/2010

Section [1] FPL - CT No. 6A through 6E

Emissions Unit Control Equipment/Method: Control 1 of 2

1.	Control Equipment/Method Description: Natural Gas: Low NOx combustion technology
2.	Control Device or Method Code: 205
<u>En</u>	nissions Unit Control Equipment/Method: Control 2 of 2
1.	Control Equipment/Method Description: Distillate Fuel Oil: Water Injection Ultra-low Sulfur Fuel
2.	Control Device or Method Code: 028, 148
En	nissions Unit Control Equipment/Method: Control of
1.	Control Equipment/Method Description:
2.	Control Device or Method Code:
<u>En</u>	nissions Unit Control Equipment/Method: Control of
1.	Control Equipment/Method Description:
2.	Control Device or Method Code:

Section [1] FPL - CT No. 6A through 6E

B. EMISSIONS UNIT CAPACITY INFORMATION

(Optional for unregulated emissions units.)

Emissions Unit Operating Capacity and Schedule

1.	Maximum Process or Throughp	out Rate:	
2.	Maximum Production Rate:		
3.	Maximum Heat Input Rate:	million Btu/hr	
4.	Maximum Incineration Rate:	pounds/hr	
		tons/day	
5.	Requested Maximum Operating	Schedule:	
		24 hours/day	7 days/week
		52 weeks/year	3,390 hours/year
6.	Operating Capacity/Schedule C See Tables S-A-1 and GE-A-1 for Tables S-A-2 and GE-A-2 for man	omment: r maximum heat input when f	iring natural gas; and
5.	See Tables S-A-1 and GE-A-1 for	omment: r maximum heat input when f	iring natural gas; and
<u> </u>	See Tables S-A-1 and GE-A-1 for	omment: r maximum heat input when f	iring natural gas; and
<u></u> б.	See Tables S-A-1 and GE-A-1 for	omment: r maximum heat input when f	iring natural gas; and
6.	See Tables S-A-1 and GE-A-1 for	omment: r maximum heat input when f	iring natural gas; and
5.	See Tables S-A-1 and GE-A-1 for	omment: r maximum heat input when f	iring natural gas; and
6.	See Tables S-A-1 and GE-A-1 for	omment: r maximum heat input when f	iring natural gas; and
5.	See Tables S-A-1 and GE-A-1 for	omment: r maximum heat input when f	iring natural gas; and
	See Tables S-A-1 and GE-A-1 for	omment: r maximum heat input when f	iring natural gas; and

Section [1] FPL - CT No. 6A through 6E

C. EMISSION POINT (STACK/VENT) INFORMATION

(Optional for unregulated emissions units.)

Emission Point Description and Type

1.	Identification of Point on Plot Plan or Flow Diagram:		2. Emission Point?	Гуре Code:				
	3. Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking: The combustion gases exhaust through a 80-ft stack. 4. ID Numbers or Descriptions of Emission Units with this Emission Point in Common:							
5.	Discharge Type Code: V	6. Stack Height 80 feet	:	7. Exit Diameter: 23 feet				
8.	Exit Temperature: See Air Report°F	9. Actual Volumetric Flow Rate: See Air Report acfm		10. Water Vapor: %				
11.	11. Maximum Dry Standard Flow Rate: dscfm		12. Nonstack Emission Point Height: feet					
13.	Emission Point UTM Coo Zone: East (km): North (km)		14. Emission Point Latitude/Longitude Latitude (DD/MM/SS) Longitude (DD/MM/SS)					
15.	Emission Point Comment: See Tables GE-A-1 and S-A firing natural gas and ultra	A-1 for the stack pa	aramenters associated					

Section [1] FPL - CT No. 6A through 6E

D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment	Description	and Rate:	Segment 1	of 2

1.	Segment Description (Pro- Internal Combustion Engin	* * <i>'</i>		Oil (Diesel);Turbine		
2.	Source Classification Cod 2-01-001-01	e (SCC):	3. SCC Units: 1,000 Gallor			
4.	Maximum Hourly Rate: 81.6	5. Maximum . 40,816	Annual Rate:	6. Estimated Annual Activity Factor:		
7.	Maximum % Sulfur: 0.0015	8. Maximum (% Ash:	9. Million Btu per SCC Unit: 131		
10.	0. Segment Comment: Million British thermal units (Btu) per SCC unit =131. Based on 7.1 lb/gal; LHV = 18,300 Btu/lb ISO conditions. Max hourly rate based on 35 F and 500 hours per year operation. Based on GE Units per CT. Data shown for Siemens F5. See Table GE-A-1 and S-A-1 in Air Permit Application Report. Note: Fuel use will vary by CT vendor.					
~						

Se	Segment Description and Rate: Segment 2 of 2						
1.							
2.	2. Source Classification Code (SCC): 2-01-002-01 3. SCC Units: Million Cubic Feet Burned				et Burned		
4.	Maximum Hourly Rate: 11.3	5.	Maximum <i>1</i> 98,669	Annual Rate:	1	Estimated Annual Activity Factor:	
7.	Maximum % Sulfur:	8.	Maximum 9	% Ash:		Million Btu per SCC Unit: 918	
10.	10. Segment Comment: Based on 918 Btu/cf (LHV). Max hourly rate based on 75 F. Max annual rate based on 75 F and 8,760 hr/yr operation. Information shown for Siemens F5 CT. See Tables GE-A-1 and S-A-1 in Air Report. Note: Fuel use will vary by CT vendor.						

Section [1]

FPL - CT No. 6A through 6E

E. EMISSIONS UNIT POLLUTANTS

List of Pollutants Emitted by Emissions Unit

1.	Pollutant Emitted	2. Primary Control	3. Secondary Control	4. Pollutant
		Device Code	Device Code	Regulatory Code
	NOx	205, 028		EL
	CO			EL
	SO2	148		EL
	VOC	-		EL
	PM			EL
	PM10			EL
	SAM	148		EL
\vdash			_	
<u> </u>				

POLLUTANT DETAIL INFORMATION
Page [1] of [6]
Nitrogen Oxides

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted: NOx	2. Total Percent Efficiency of Control:			
3. Potential Emissions: See Air Report Ib/hour See Air Report	t tons/year	•	etically Limited?	
5. Range of Estimated Fugitive Emissions (as to tons/year	s applicable):		<u>-</u>	
6. Emission Factor: See Air Report			7. Emissions Method Code:	
Reference:				
8.a. Baseline Actual Emissions (if required):	8.b. Baseline 2	24-month	Period:	
tons/year	From:	T	o:	
9.a. Projected Actual Emissions (if required):	9.b. Projected	Monitori	ng Period:	
tons/year	☐ 5 year	rs 🔲 10) years	
10. Calculation of Emissions: See Air Report, Appendix C in Air Report for and S-A-2 for Siemens; Tables GE-A-1 and G	GE-A-2 for GE.	emissions	s. Tables S-A-1	
11. Potential, Fugitive, and Actual Emissions Comment:				

POLLUTANT DETAIL INFORMATION Page [1] of [6] Nitrogen Oxides

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:							
3.	Allowable Emissions and Units: See Air Report; Table 4-1	4. Equivalent Allowable Emissions: See Air Report lb/hour See Air Report tons/year							
5.	Method of Compliance: See Air Report, Table 4-1								
6.	6. Allowable Emissions Comment (Description of Operating Method):								
<u>Al</u>	lowable Emissions Allowable Emissions	of							
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:							
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year							
	Method of Compliance:								
6.	6. Allowable Emissions Comment (Description of Operating Method):								
Al	owable Emissions Allowable Emissions	of							
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:							
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year							
5.	Method of Compliance:								
6.	Allowable Emissions Comment (Description	of Operating Method):							

POLLUTANT DETAIL INFORMATION
Page [2] of [6]
Carbon Monoxide

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1 5 1 1	0 55 15 15	
Pollutant Emitted: Carbon Monoxide- CO	2. Total Percent Eff	iciency of Control:
3. Potential Emissions:	4. Sy	nthetically Limited?
See Air Report lb/hour See Air Report	t tons/year	Yes 🛛 No
5. Range of Estimated Fugitive Emissions (as	applicable):	
to tons/year	_	
6. Emission Factor: See Air Report		7. Emissions
D. C		Method Code:
Reference:		
8.a. Baseline Actual Emissions (if required):	8.b. Baseline 24-mo	nth Period:
tons/year	From:	To:
9.a. Projected Actual Emissions (if required):	9.b. Projected Monit	oring Period:
tons/year	☐ 5 years ☐	10 years
10. Calculation of Emissions: See Air Report, Appendix C for baseline actu Siemens; Tables GE-A-1 and GE-A-2 for GE.		S-A-1 and S-A-2 for
11. Potential, Fugitive, and Actual Emissions Co	omment:	

POLLUTANT DETAIL INFORMATION Page [2] of [6] Carbon Monoxide

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:							
3.	Allowable Emissions and Units: See Air Report; Table 4-1	4. Equivalent Allowable Emissions: See Air Report lb/hour See Air Report tons/year							
5.	Method of Compliance: See Air Report, Table 4-1								
6.	6. Allowable Emissions Comment (Description of Operating Method):								
<u>Al</u>	owable Emissions Allowable Emissions	of							
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:							
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year							
5.	Method of Compliance:								
6.	6. Allowable Emissions Comment (Description of Operating Method):								
<u>All</u>	owable Emissions Allowable Emissions	of							
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:							
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year							
	Method of Compliance:								
6.	Allowable Emissions Comment (Description	of Operating Method):							

POLLUTANT DETAIL INFORMATION
Page [3] of [6]
Sulfur Dioxide

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1. Pollutant Emitted: Sulfur Dioxide - SO2	2. Total Percent Efficiency of Control:		
3. Potential Emissions: See Air Report lb/hour See Air Report	t tons/year	4. Synth ☐ Y	netically Limited? es 🛛 No
5. Range of Estimated Fugitive Emissions (as to tons/year	s applicable):		
6. Emission Factor: See Air Report			7. Emissions Method Code:
Reference:			
8.a. Baseline Actual Emissions (if required):	8.b. Baseline	24-month	Period:
tons/year	From:	T	o:
9.a. Projected Actual Emissions (if required):	9.b. Projected	Monitori	ng Period:
tons/year	☐ 5 year	rs 🔲 10) years
10. Calculation of Emissions: See Air Report, Appendix C for baseline actu Siemens; Tables GE-A-1 and GE-A-2 for GE.		Γables S-A	-1 and S-A-2 for
11. Potential, Fugitive, and Actual Emissions Co	omment:		

POLLUTANT DETAIL INFORMATION Page [3] of [6] Sulfur Dioxide

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions 1 of 1

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:							
3.	Allowable Emissions and Units: See Air Report; Table 4-1	4. Equivalent Allowable Emissions: See Air Report lb/hour See Air Report tons/yea							
5.	Method of Compliance: See Air Report, Table 4-1	·							
6.	6. Allowable Emissions Comment (Description of Operating Method):								
Al	lowable Emissions Allowable Emissions	of							
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:							
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year							
	Method of Compliance:								
6.	Allowable Emissions Comment (Description	of Operating Method):							
All	lowable Emissions Allowable Emissions	of							
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:							
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year							
5.	Method of Compliance:								
6.	Allowable Emissions Comment (Description	of Operating Method):							

POLLUTANT DETAIL INFORMATION
Page [4] of [6]
Volatile Organic Compounds

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:	2. Total Percent Efficiency of Control:				
Volatile Organic Compounds - VOC			·		
3. Potential Emissions:		_	netically Limited?		
See Air Report lb/hour See Air Report	t tons/year	□ Y	es 🛛 No		
5. Range of Estimated Fugitive Emissions (as	applicable):				
to tons/year					
6. Emission Factor: See Air Report			7. Emissions		
D.C			Method Code:		
Reference:					
8.a. Baseline Actual Emissions (if required):	8.b. Baseline				
tons/year	From:		0:		
9.a. Projected Actual Emissions (if required):	9.b. Projected	l Monitori	ng Period:		
tons/year	☐ 5 yea	rs 🗌 10) years		
10. Calculation of Emissions: See Air Report, Appendix C for baseline actu Siemens; Tables GE-A-1 and GE-A-2 for GE.		Γables S-A	-1 and S-A-2 for		
11. Potential, Fugitive, and Actual Emissions Comment:					

Section [1] FPL - CT No. 6A through 6E

POLLUTANT DETAIL INFORMATION Page [4] of [6] Volatile Organic Compounds

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:		
3.	Allowable Emissions and Units: See Air Report; Table 4-1	4. Equivalent Allowable Emissions: See Air Report lb/hour See Air Report tons/year		
5.	5. Method of Compliance: See Air Report, Table 4-1			
6. Allowable Emissions Comment (Description of Operating Method):				
Al	lowable Emissions Allowable Emissions	of		
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5.	5. Method of Compliance:			
6.	6. Allowable Emissions Comment (Description of Operating Method):			
All	owable Emissions Allowable Emissions	of		
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5.	5. Method of Compliance:			
6.	6. Allowable Emissions Comment (Description of Operating Method):			

POLLUTANT DETAIL INFORMATION
Page [5] of [6]
Particulate Matter - PM

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted: Particulate Matter - PM	2. Total Percent Efficie	ency of Control:
3. Potential Emissions: See Air Report lb/hour See Air Report	1	netically Limited? es 🛛 No
5. Range of Estimated Fugitive Emissions (as to tons/year	applicable):	
6. Emission Factor: See Air Report		7. Emissions Method Code:
Reference:		
8.a. Baseline Actual Emissions (if required):	8.b. Baseline 24-month	Period:
tons/year	From:	o:
9.a. Projected Actual Emissions (if required):	9.b. Projected Monitoria	ng Period:
tons/year	_) years
10. Calculation of Emissions: See Air Report, Appendix C for baseline actu Siemens; Tables GE-A-1 and GE-A-2 for GE.		-1 and S-A-2 for
11. Potential, Fugitive, and Actual Emissions Co	omment:	

POLLUTANT DETAIL INFORMATION Page [5] of [6] Particulate Matter - PM

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:		
3.	Allowable Emissions and Units: See Air Report; Table 4-1	4. Equivalent Allowable Emissions: See Air Report lb/hour See Air Report tons/year		
5.	. Method of Compliance: See Air Report, Table 4-1			
6.	6. Allowable Emissions Comment (Description of Operating Method):			
<u>Al</u>	lowable Emissions Allowable Emissions	of		
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5.	5. Method of Compliance:			
6.	6. Allowable Emissions Comment (Description of Operating Method):			
Al	owable Emissions Allowable Emissions	of		
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5.	Method of Compliance:			
6.	Allowable Emissions Comment (Description	of Operating Method):		

POLLUTANT DETAIL INFORMATION
Page [6] of [6]
Particulate Matter - PM10

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1. Pollutant Emitted: PM10	2. Total Percent Effic	iency of Control:	
3. Potential Emissions: See Air Report lb/hour See Air Report		thetically Limited? Yes 🛛 No	
5. Range of Estimated Fugitive Emissions (as to tons/year	s applicable):		
6. Emission Factor: See Air Report Reference:		7. Emissions Method Code:	
8.a. Baseline Actual Emissions (if required):	8.b. Baseline 24-mont	h Period:	
tons/year	From:	Го:	
9.a. Projected Actual Emissions (if required):	9.b. Projected Monitor	ring Period:	
tons/year	☐ 5 years ☐ 1	10 years	
tons/year			
11. Potential, Fugitive, and Actual Emissions Comment:			

POLLUTANT DETAIL INFORMATION Page [6] of [6] Particulate Matter - PM10

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:		
3.	Allowable Emissions and Units: See Air Report; Table 4-1	4. Equivalent Allowable Emissions: See Air Report lb/hour See Air Report tons/year		
5.	Method of Compliance: See Air Report, Table 4-1			
6.	6. Allowable Emissions Comment (Description of Operating Method):			
<u>Al</u>	lowable Emissions Allowable Emissions	of		
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5.	Method of Compliance:			
6.	6. Allowable Emissions Comment (Description of Operating Method):			
All	lowable Emissions Allowable Emissions	of		
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5.	Method of Compliance:			
6.	6. Allowable Emissions Comment (Description of Operating Method):			

Section [1] FPL - CT No. 6A through 6E

G. VISIBLE EMISSIONS INFORMATION

Complete Subsection G if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

Visible Emissions Limitation: Visible Emissions Limitation 1 of 2

1.	Visible Emissions Subtype: VE20	2. Basis for Allowable (☑ Rule	Dpacity: Other
<u> </u>			
3.	Allowable Opacity:	10 10	400 0/
		cceptional Conditions:	100 %
	Maximum Period of Excess Opacity Allowe	ea: 	60 min/hour
4.	Method of Compliance: EPA Method 9		
5.	Visible Emissions Comment:		
	FDEP Rule 62-296.320(4)(b)1, F.A.C., requires provided by Rule 62-210.700(1).	s 20 percent opacity. Exce	ss emissions
Vis	sible Emissions Limitation: Visible Emissi		
1.	Visible Emissions Subtype: VE10	2. Basis for Allowable (☐ Rule	Opacity: ☑ Other
3.	Allowable Opacity:		<u>—</u>
].	1 7	ceptional Conditions:	%
	Maximum Period of Excess Opacity Allowe	-	min/hour
4.	Method of Compliance: EPA Method 9		
4.	Method of Comphance. EFA method 9		
5.	Visible Emissions Comment:		
	Proposed as emission limit for PM/PM ₁₀ .		

Section [1] FPL - CT No. 6A through 6E

H. CONTINUOUS MONITOR INFORMATION

Complete Subsection H if this emissions unit is or would be subject to continuous monitoring.

Continuous Monitoring System: Continuous Monitor 1 of 2

1.	Parameter Code: EM	2.	Pollutant(s): NOX
3.	CMS Requirement:	\boxtimes	Rule
4.	Monitor Information Manufacturer:		
	Model Number:		Serial Number:
5.	Installation Date:	6.	Performance Specification Test Date:
7.	Continuous Monitor Comment:		
	Monitoring is also required pursuant to 40 Cl Subpart KKKK.	FR 7	5 or continuous monitoring using
Co	ntinuous Monitoring System: Continuous	Mor	nitor 2 of 2
1.	Parameter Code:	2.	Pollutant(s):
3.	CMS Requirement:		Rule
4.	Monitor Information Manufacturer:		
	Model Number:		Serial Number:
5.	Installation Date:	6.	Performance Specification Test Date:
7.	Continuous Monitor Comment:		-
	-		

Section [1] FPL - CT No. 6A through 6E

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: See Air Reports Previously Submitted, Date
2.	Fuel Analysis or Specification: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: See Air Reports Previously Submitted, Date
3.	Detailed Description of Control Equipment: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: See Air Reports Previously Submitted, Date
4.	Procedures for Startup and Shutdown: (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Previously Submitted, Date
	Not Applicable (construction application)
5.	Operation and Maintenance Plan: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Previously Submitted, Date Not Applicable
6.	Compliance Demonstration Reports/Records: Attached, Document ID:
	Test Date(s)/Pollutant(s) Tested:
	☐ Previously Submitted, Date:
	Test Date(s)/Pollutant(s) Tested:
	☐ To be Submitted, Date (if known):
	Test Date(s)/Pollutant(s) Tested:
	Not Applicable Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute: Attached, Document ID: Not Applicable

Section [1] FPL - CT No. 6A through 6E

I. EMISSIONS UNIT ADDITIONAL INFORMATION (CONTINUED)

Additional Requirements for Air Construction Permit Applications

1.	
	F.A.C.; 40 CFR 63.43(d) and (e)):
	Attached, Document ID: <u>See Air Reports</u> Not Applicable
2.	
	212.500(4)(f), F.A.C.):
	Attached, Document ID: <u>See Air Reports</u> Not Applicable
3.	Description of Stack Sampling Facilities: (Required for proposed new stack sampling facilities only)
	Attached, Document ID: <u>See Air Reports</u> Not Applicable
<u>A</u>	dditional Requirements for Title V Air Operation Permit Applications
1.	Identification of Applicable Requirements:
	Attached, Document ID:
2.	Compliance Assurance Monitoring:
	☐ Attached, Document ID: ⊠ Not Applicable
3.	Alternative Methods of Operation:
	☐ Attached, Document ID: ☐ Not Applicable
4.	Alternative Modes of Operation (Emissions Trading):
	☐ Attached, Document ID: ⊠ Not Applicable
	Iditional Descriptions and Comment
At	Aditional Requirements Comment

Section [2] FPL - Black-Start Engines

III. EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Application - For Title V air operation permitting only, emissions units are classified as regulated, unregulated, or insignificant. If this is an application for an initial, revised or renewal Title V air operation permit, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each regulated and unregulated emissions unit addressed in this application. Some of the subsections comprising the Emissions Unit Information Section of the form are optional for unregulated emissions units. Each such subsection is appropriately marked. Insignificant emissions units are required to be listed at Section II, Subsection C.

Air Construction Permit or FESOP Application - For air construction permitting or federally enforceable state air operation permitting, emissions units are classified as either subject to air permitting or exempt from air permitting. The concept of an "unregulated emissions unit" does not apply. If this is an application for an air construction permit or FESOP, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air permitting are required to be listed at Section II, Subsection C.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit Application – Where this application is used to apply for both an air construction permit and a revised or renewal Title V air operation permit, each emissions unit is classified as either subject to air permitting or exempt from air permitting for air construction permitting purposes, and as regulated, unregulated, or insignificant for Title V air operation permitting purposes. A separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit addressed in this application that is subject to air construction permitting and for each such emissions unit that is a regulated or unregulated unit for purposes of Title V permitting. (An emissions unit may be exempt from air construction permitting but still be classified as an unregulated unit for Title V purposes.) Emissions units classified as insignificant for Title V purposes are required to be listed at Section II, Subsection C.

If submitting the application form in hard copy, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application must be indicated in the space provided at the top of each page.

DEP Form No. 62-210.900(1) Effective: 03/11/2010

Section [2] FPL - Black-Start Engines

A. GENERAL EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Emissions Unit Classification

1.	Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)					
			missions Unit Informati	on Section is a regulated		
	emissions unit	unit addressed in this E	missions Unit Informati	on Section is an		
	unregulated en		missions Omt miornati	on section is an		
En	nissions Unit Desc	ription and Status	-			
1.	Type of Emissions	Unit Addressed in this	Section: (Check one)			
	single process	s Unit Information Secti or production unit, or ac which has at least one d	tivity, which produces	one or more air		
	of process or p		vities which has at least	e emissions unit, a group one definable emission		
		s Unit Information Section production units and a		e emissions unit, one or fugitive emissions only.		
2.	 Description of Emissions Unit Addressed in this Section: Four Black-Start Engines. 					
3.	Emissions Unit Ide	entification Number:				
4.	Emissions Unit	5. Commence	6. Initial Startup	7. Emissions Unit		
	Status Code:	Construction Date:	Date:	Major Group SIC Code:		
	Α	2014	2016	49		
8.	Federal Program A	applicability: (Check all	that apply)			
	☐ Acid Rain Uni	t				
	☐ CAIR Unit					
9.	Package Unit:					
L_	Manufacturer:		Model Number:			
	10. Generator Nameplate Rating: MW/CT					
11.	11. Emissions Unit Comment:					

Section [2] FPL - Black-Start Engines

Emissions Unit Control Equipment/Method: Control of
1. Control Equipment/Method Description:
2 Com 1D : Malado 1
2. Control Device or Method Code:
Emissions Unit Control Equipment/Method: Control of
1. Control Equipment/Method Description:
2 Com 1D : Mai 10 1
2. Control Device or Method Code:
Emissions Unit Control Equipment/Method: Control of
1. Control Equipment/Method Description:
2. Control Device or Method Code:
Emissions Unit Control Equipment/Method: Control of
1. Control Equipment/Method Description:
2. Control Device or Method Code:

Section [2] FPL - Black-Start Engines

B. EMISSIONS UNIT CAPACITY INFORMATION

(Optional for unregulated emissions units.)

Emissions Unit Operating Capacity and Schedule

1.	. Maximum Process or Throughput Rate:		
2.	Maximum Production Rate:		
3.	Maximum Heat Input Rate: 116	million Btu/hr	
4.	Maximum Incineration Rate:	pounds/hr	
		tons/day	
5.	Requested Maximum Operating	Schedule:	
		hours/day	days/week
		weeks/year	100 hours/year
6.	Operating Capacity/Schedule Co. 29 MMBtu/hr for each engines	mment:	·

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Section [2]

FPL - Black-Start Engines

C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

Emission Point Description and Type

Identification of Point on Plot Plan or Flow Diagram:		2. Emission Point 7	Гуре Code: 	
Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking: 4. ID Numbers or Descriptions of Emission Units with this Emission Point in Common:				
5. Discharge Type Code: V	6. Stack Height 30 feet	•	7. Exit Diameter: 2 feet	
8. Exit Temperature: 893°F			10. Water Vapor: %	
11. Maximum Dry Standard F dscfm	11. Maximum Dry Standard Flow Rate: 12. Nonstack Emission Point Height: feet			
13. Emission Point UTM Coordinates Zone: East (km): Latitude (DD/MM/SS) North (km): Longitude (DD/MM/SS)		M/SS)		
15. Emission Point Comment: Stack parameters for one		<u> </u>		

Section [2]

FPL - Black-Start Engines

D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment Description and Rate: Segment 1 of 1

1. Segment Description (Process/Fuel Type):

Internal Combustion Engines; Electric Generation; Distillate Oil (Diesel);Turbine				
2. Source Classification Code (SCC): 2-01-001-01 3. SCC Units: 1,000 Gallons burned				
ım Hourly Rate:	5. Maximum 21.1	Annual Rate:	6. Estimated Annual Activity Factor:	
ım % Sulfur:	8. Maximum	% Ash:	9. Million Btu per SCC Unit: 137.7	
10. Segment Comment: Max hourly rate=29.01 MMBtu/hr / (137.7 MMBtu/kgal)=0.211 kgal/hr Max annual rate=0.211 kgal/hr x 100 hr/yr=21.1 kgal/yr				
escription and Ra	ate: Segment_	of		
1. Segment Description (Process/Fuel Type):				
Classification Code	e (SCC):	3. SCC Units	:	
m Hourly Rate:	5. Maximum	Annual Rate:	6. Estimated Annual Activity Factor:	
ım % Sulfur:	8. Maximum	% Ash:	9. Million Btu per SCC Unit:	
t Comment:				
	Classification Cod 1-01 Im Hourly Rate: Im % Sulfur: It Comment: Irly rate=29.01 MM It all rate=0.211 kga Escription and Rate It Description (Pro	Classification Code (SCC): 1-01 Im Hourly Rate: 5. Maximum 21.1 Im % Sulfur: 8. Maximum It Comment: Irly rate=29.01 MMBtu/hr / (137.7 MM) It comment: Irly rate=29.01 kgal/hr x 100 hr/yr=2 Escription and Rate: Segment It Description (Process/Fuel Type): Classification Code (SCC): Im Hourly Rate: 5. Maximum Im % Sulfur: 8. Maximum	Classification Code (SCC): 3. SCC Units 1,000 Gallo 1,000 Gallo	

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Section [2] FPL - Black-Start Engines

E. EMISSIONS UNIT POLLUTANTS

List of Pollutants Emitted by Emissions Unit

1. Pollutant Emitted	2. Primary Control	3. Secondary Control	4. Pollutant
	Device Code	Device Code	Regulatory Code
NOx			EL
СО			EL
SO2	Fuel Quality		EL
VOC			EL
PM			EL
PM10			EL
		-	
	_		

POLLUTANT DETAIL INFORMATION
Page [1] of [6]
Nitrogen Oxides

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted: NOx	2. Total Percent Effici	ency of Control:
3. Potential Emissions: 47.6 lb/hour 2.4	4. Synt Stons/year	hetically Limited? Yes
5. Range of Estimated Fugitive Emissions (as to tons/year	s applicable):	
6. Emission Factor: 5.2 g/hr-hr Reference: Manufacturer information		7. Emissions Method Code: 2
8.a. Baseline Actual Emissions (if required):	8.b. Baseline 24-month	Deriod:
tons/year		To:
·		
9.a. Projected Actual Emissions (if required): tons/year	9.b. Projected Monitor	Č
·	\Box 5 years \Box 1	0 years
10. Calculation of Emissions: 5.2 g/hp-hr x 4,157 hp x 1 lb/453.6 g = 47.6 lb/ 47.6 lb/hr x 100 hr x 1 ton/2,000 lb = 2.4 TPY		
11. Potential, Fugitive, and Actual Emissions Commissions are for one generator.	omment:	

POLLUTANT DETAIL INFORMATION Page [1] of [6] Nitrogen Oxides

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:			
3.	Allowable Emissions and Units: Subpart IIII NSPS	4. Equivalent Allowable Emissions: 47.6 lb/hour 2.4 tons/year			
5.	Method of Compliance: Manufacturer certification of applicable Subpart IIII standards.				
6.	Allowable Emissions Comment (Description	of Operating Method):			
Al	lowable Emissions Allowable Emissions	of			
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year			
5.	Method of Compliance:				
6.	Allowable Emissions Comment (Description	of Operating Method):			
Al	lowable Emissions Allowable Emissions	of			
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: 1b/hour tons/year			
5.	Method of Compliance:				
6.	6. Allowable Emissions Comment (Description of Operating Method):				

POLLUTANT DETAIL INFORMATION
Page [2] of [6]
Carbon Monoxide

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Total Land Land Land Land Land Land Land Land	• x x • j • • • • • · · · · · · ·		SIGIIS
1. Pollutant Emitted: CO	2. Total Percent Efficiency of Control:		ency of Control:
3. Potential Emissions:		4. Synth	netically Limited?
	tons/year	⊠ Y	=
5. Range of Estimated Fugitive Emissions (as	s applicable):		
to tons/year	· · · · · · · · · · · · · · · · · · ·		
6. Emission Factor: 0.7 g/hr-hr			7. Emissions
			Method Code:
Reference: Manufacturer informaton			2
8.a. Baseline Actual Emissions (if required):	8.b. Baseline	24-month	Period:
tons/year	From:	T	o:
9.a. Projected Actual Emissions (if required):	9.b. Projected	Monitoria	ng Period:
tons/year	☐ 5 year	rs 🗌 10) years
10. Calculation of Emissions: 0.7 g/hp-hr x 4,157 hp x 1 lb/453.6 g = 6.0 lb/h 6.0 lb/hr x 100 hr x 1 ton/2,000 lb = 0.3 TPY 11. Potential, Fugitive, and Actual Emissions Calculations are for one generator.			

POLLUTANT DETAIL INFORMATION Page [2] of [6] Carbon Monoxide

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:			
3.	Allowable Emissions and Units: Subpart IIIi NSPS	4. Equivalent Allowable Emissions: 6.0 lb/hour 0.3 tons/year			
5.	Method of Compliance: Manufacturer certification of applicable Subp	art IIII standards.			
6.	Allowable Emissions Comment (Description	of Operating Method):			
Al	lowable Emissions Allowable Emissions	of			
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year			
5.	Method of Compliance:				
6.	Allowable Emissions Comment (Description	of Operating Method):			
Al	lowable Emissions Allowable Emissions	of			
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year			
5.	Method of Compliance:				
6.	Allowable Emissions Comment (Description	of Operating Method):			

POLLUTANT DETAIL INFORMATION Page [3] of [6] Sulfur Dioxide

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted: Sulfur Dioxide - SO2	2. Total Perc	ent Efficie	ency of Control:
3. Potential Emissions: 0.045 lb/hour 0.0022	tons/year	4. Synth ⊠ Y	netically Limited? es
5. Range of Estimated Fugitive Emissions (as to tons/year	s applicable):		
6. Emission Factor: 0.0015% S fuel oil Reference: FPL, 2013			7. Emissions Method Code: 2
8.a. Baseline Actual Emissions (if required): tons/year	8.b. Baseline From:	T	o:
9.a. Projected Actual Emissions (if required): tons/year	9.b. Projected ☐ 5 year		ng Period:) years
10. Calculation of Emissions: 0.0015% S x 64/32 x 7.1 lb/gal x 210.7 gal/hr = 0.045 lb/hr x 100 hr x 1 ton/2,000 lb = 0.0022 T	ГРҮ		
11. Potential, Fugitive, and Actual Emissions Co Emissions are for one generator.	omment:		

POLLUTANT DETAIL INFORMATION Page [3] of [6] Sulfur Dioxide

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:			
3.	Allowable Emissions and Units: 0.0015% S fuel oil	4. Equivalent Allowable Emissions: 0.045 lb/hour 0.0022 tons/year			
5.	Method of Compliance: Fuel vendor information				
6.	Allowable Emissions Comment (Description	of Operating Method):			
Al	lowable Emissions Allowable Emissions	of			
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year			
5.	Method of Compliance:				
6.	6. Allowable Emissions Comment (Description of Operating Method):				
All	lowable Emissions Allowable Emissions	of			
1.	Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:			
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year			
5.	Method of Compliance:				
6.	6. Allowable Emissions Comment (Description of Operating Method):				

POLLUTANT DETAIL INFORMATION
Page [4] of [6]
Volatile Organic Compounds

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted: VOC	2. Total Perc	ent Efficie	ency of Control:
3. Potential Emissions: 0.9 lb/hour 0.08	tons/year	4. Synth ⊠ Y	netically Limited? Yes □ No
5. Range of Estimated Fugitive Emissions (as to tons/year	s applicable):		
6. Emission Factor: 0.1 g/hr-hr Reference: Manufacturer information			7. Emissions Method Code: 2
8.a. Baseline Actual Emissions (if required): tons/year	8.b. Baseline From:		Period: To:
9.a. Projected Actual Emissions (if required): tons/year	9.b. Projected ☐ 5 yea		ng Period: 0 years
10. Calculation of Emissions: 0.1g/hp-hr x 4,157 hp x 1 lb/453.6 g = 0.9 lb/hr 0.9 lb/hr x 100 hr x 1 ton/2,000 lb = 0.05 TPY			
11. Potential, Fugitive, and Actual Emissions Co Emissions are for one generator.	omment:		

POLLUTANT DETAIL INFORMATION Page [4] of [6] Volatile Organic Compounds

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:			
3.	Allowable Emissions and Units: Subpart IIII NSPS	4. Equivalent Allowable Emissions:0.9 lb/hour 0.05 tons/year			
5.	Method of Compliance: Manufacturer certification of applicable Subp	art IIII standards.			
6.	Allowable Emissions Comment (Description	of Operating Method):			
<u>Al</u>	lowable Emissions Allowable Emissions	of			
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year			
5.	Method of Compliance:				
6.	6. Allowable Emissions Comment (Description of Operating Method):				
All	owable Emissions Allowable Emissions	of			
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year			
5.	Method of Compliance:				
6.	Allowable Emissions Comment (Description	of Operating Method):			

POLLUTANT DETAIL INFORMATION
Page [5] of [6]
Particulate Matter - PM

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1. Pollutant Emitted: PM	2. Total Percent Efficiency of Control:		
3. Potential Emissions: 0.3 lb/hour 0.01	l tons/year	4. Syntł ⊠ Y	netically Limited? es
5. Range of Estimated Fugitive Emissions (as to tons/year	applicable):		
6. Emission Factor: 0.03 g/hr-hr Reference: Manufacturer information			7. Emissions Method Code: 2
8.a. Baseline Actual Emissions (if required): tons/year	8.b. Baseline From:		Period:
9.a. Projected Actual Emissions (if required): tons/year	9.b. Projected ☐ 5 year		
10. Calculation of Emissions: 0.03g/hp-hr x 4,157 hp x 1 lb/453.6 g = 0.3 lb/hr 0.3 lb/hr x 100 hr x 1 ton/2,000 lb = 0.01 TPY 11. Potential, Fugitive, and Actual Emissions Comment:			
Emissions are for one generator.			

POLLUTANT DETAIL INFORMATION
Page [4] of [6]
Particulate Matter - PM

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions 1 of 1
--

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units: Subpart IIII NSPS	4. Equivalent Allowable Emissions: 0.3 lb/hour 0.01 tons/year	
5.	5. Method of Compliance: Manufacturer certification of applicable Subpart IIII standards.		
6. Allowable Emissions Comment (Description of Operating Method):			
Allowable Emissions of			
1.	Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year	
5.	5. Method of Compliance:		
6.	6. Allowable Emissions Comment (Description of Operating Method):		
Allowable Emissions of			
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year	
5. Method of Compliance:			
6. Allowable Emissions Comment (Description of Operating Method):			

EMISSIONS UNIT INFORMATION Section [2] FPL - Black-Start Engines

POLLUTANT DETAIL INFORMATION
Page [6] of [6]
Particulate Matter - PM10

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Potential, Estimated Fugitive, and Baseline & Projected Actual Emissions

1. Pollutant Emitted: PM10	2. Total Perc	ent Efficie	ency of Control:
3. Potential Emissions: 0.3 lb/hour 0.01	tons/year	4. Synth ⊠ Y	netically Limited? es
5. Range of Estimated Fugitive Emissions (as to tons/year	s applicable):		
6. Emission Factor: 0.03 g/hr-hr Reference: Manufacturer information			7. Emissions Method Code: 2
			_
8.a. Baseline Actual Emissions (if required):	8.b. Baseline	24-month	Period:
tons/year	From:	T	0:
9.a. Projected Actual Emissions (if required):	9.b. Projected	d Monitori	ng Period:
tons/year	☐ 5 yea	rs 🗌 10) years
10. Calculation of Emissions: 0.03 g/hp-hr x 4,157 hp x 1 lb/453.6 g = 0.3 lb/ 0.3 lb/hr x 100 hr x 1 ton/2,000 lb = 0.01 TPY			
11. Potential, Fugitive, and Actual Emissions Co Emissions are for one generator.	omment:		

EMISSIONS UNIT INFORMATION Section [2]

FPL - Black-Start Engines

POLLUTANT DETAIL INFORMATION
Page [6] of [6]
Particulate Matter - PM10

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION -

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

ALLOWABLE EMISSIONS

Allowable Emissions 1 of 1

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: Subpart IIII NSPS	4. Equivalent Allowable Emissions: 0.3 lb/hour 0.01 tons/year
5.	Method of Compliance: Manufacturer certification of Subpart IIII stand	dards.
6.	Allowable Emissions Comment (Description	n of Operating Method):
Al	lowable Emissions Allowable Emissions	of
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
	Method of Compliance:	
6.	Allowable Emissions Comment (Description	of Operating Method):
Al	owable Emissions Allowable Emissions	of
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:	
6.	Allowable Emissions Comment (Description	of Operating Method):

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FPL - Black-Start Engines

G. VISIBLE EMISSIONS INFORMATION

Complete Subsection G if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

<u>Visible Emissions Limitation:</u> Visible Emissions Limitation <u>1</u> of <u>1</u>

1.	Visible Emissions Subtype: VE20	2. Basis for Allowable C ⊠ Rule	pacity: Other
3.	Allowable Opacity: Normal Conditions: 20 % Ex Maximum Period of Excess Opacity Allower	ceptional Conditions:	100 % 60 min/hour
4.	Method of Compliance: DEP Method 9		
5.	Visible Emissions Comment: Rule 62-296.320(4)(b)1., F.A.C. requires 20 per Rule 62-210.700(1).	ercent opacity. Excess emi	ssions provided by
Vis	sible Emissions Limitation: Visible Emission	ons Limitation of	
1.	Visible Emissions Subtype:	2. Basis for Allowable O ☐ Rule	pacity: Other
	Maximum Period of Excess Opacity Allowe	ceptional Conditions:	% min/hour
4.	Method of Compliance:		
5.	Visible Emissions Comment:		

Section [2] FPL - Black-Start Engines

H. CONTINUOUS MONITOR INFORMATION

Complete Subsection H if this emissions unit is or would be subject to continuous monitoring.

$\overline{\mathbf{c}}$	ontinuous Monitoring System: Continuous	
1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	⊠ Rule ☐ Other
4.	Monitor Information	
	Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	-
	<u> </u>	
<u>Co</u>	ntinuous Monitoring System: Continuous	Monitor of
	Parameter Code: Continuous	Monitor of 2. Pollutant(s):
1.	Parameter Code:	2. Pollutant(s):
3.	Parameter Code: CMS Requirement: Monitor Information	2. Pollutant(s):
3. 4.	Parameter Code: CMS Requirement: Monitor Information Manufacturer:	2. Pollutant(s): Rule Other
 3. 4. 	Parameter Code: CMS Requirement: Monitor Information Manufacturer: Model Number:	2. Pollutant(s): □ Rule □ Other Serial Number:
 3. 4. 	Parameter Code: CMS Requirement: Monitor Information Manufacturer: Model Number: Installation Date:	2. Pollutant(s): □ Rule □ Other Serial Number:
 3. 4. 	Parameter Code: CMS Requirement: Monitor Information Manufacturer: Model Number: Installation Date:	2. Pollutant(s): □ Rule □ Other Serial Number:
 3. 4. 	Parameter Code: CMS Requirement: Monitor Information Manufacturer: Model Number: Installation Date:	2. Pollutant(s): □ Rule □ Other Serial Number:
 3. 4. 	Parameter Code: CMS Requirement: Monitor Information Manufacturer: Model Number: Installation Date:	2. Pollutant(s): □ Rule □ Other Serial Number:

Section [2] FPL - Black-Start Engines

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: See Air Reports Previously Submitted, Date
2.	Fuel Analysis or Specification: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: See Air Reports Previously Submitted, Date
3.	Detailed Description of Control Equipment: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) ✓ Attached, Document ID: See Air Reports ☐ Previously Submitted, Date
4.	Procedures for Startup and Shutdown: (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Previously Submitted, Date
	Not Applicable (construction application)
5.	Operation and Maintenance Plan: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Previously Submitted, Date Not Applicable
6.	Compliance Demonstration Reports/Records:
	Attached, Document ID:
	Test Date(s)/Pollutant(s) Tested:
	☐ Previously Submitted, Date:
	Test Date(s)/Pollutant(s) Tested:
	To be Calmitted Date (film and)
	To be Submitted, Date (if known): Test Date(s)/Pollutant(s) Tested:
	Test Date(s)/1 officialit(s) Tested.
	Not Applicable Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute: Attached, Document ID: Not Applicable

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Section [2] FPL - Black-Start Engines

I. EMISSIONS UNIT ADDITIONAL INFORMATION (CONTINUED)

Additional Requirements for Air Construction Permit Applications

1.	Control Technology Review and Analysis (Rules 62-212.400(10) and 62-212.500(7),			
	F.A.C.; 40 CFR 63.43(d) and (e)):			
2.	Good Engineering Practice Stack Height Analysis (Rules 62-212.400(4)(d) and 62-			
	212.500(4)(f), F.A.C.):			
	☐ Attached, Document ID: ⊠ Not Applicable			
3.	Description of Stack Sampling Facilities: (Required for proposed new stack sampling facilities			
	only)			
	☐ Attached, Document ID: Not Applicable			
Ac	dditional Requirements for Title V Air Operation Permit Applications			
1.	Identification of Applicable Requirements: Attached, Document ID:			
2.	Compliance Assurance Monitoring: ☐ Attached, Document ID: ☐ Not Applicable			
3.	Alternative Methods of Operation: Attached, Document ID: Not Applicable			
4.	Alternative Modes of Operation (Emissions Trading):			
	☐ Attached, Document ID: ☐ ☐ Not Applicable			
Ad	Iditional Requirements Comment			
1				

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Section [3] FPL - Fuel Tanks

III. EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Application - For Title V air operation permitting only, emissions units are classified as regulated, unregulated, or insignificant. If this is an application for an initial, revised or renewal Title V air operation permit, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each regulated and unregulated emissions unit addressed in this application. Some of the subsections comprising the Emissions Unit Information Section of the form are optional for unregulated emissions units. Each such subsection is appropriately marked. Insignificant emissions units are required to be listed at Section II, Subsection C.

Air Construction Permit or FESOP Application - For air construction permitting or federally enforceable state air operation permitting, emissions units are classified as either subject to air permitting or exempt from air permitting. The concept of an "unregulated emissions unit" does not apply. If this is an application for an air construction permit or FESOP, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air permitting are required to be listed at Section II, Subsection C.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit Application – Where this application is used to apply for both an air construction permit and a revised or renewal Title V air operation permit, each emissions unit is classified as either subject to air permitting or exempt from air permitting for air construction permitting purposes, and as regulated, unregulated, or insignificant for Title V air operation permitting purposes. A separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit addressed in this application that is subject to air construction permitting and for each such emissions unit that is a regulated or unregulated unit for purposes of Title V permitting. (An emissions unit may be exempt from air construction permitting but still be classified as an unregulated unit for Title V purposes.) Emissions units classified as insignificant for Title V purposes are required to be listed at Section II, Subsection C.

If submitting the application form in hard copy, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application must be indicated in the space provided at the top of each page.

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EMISSIONS UNIT INFORMATION Section [3] FPL - Fuel Tanks

A. GENERAL EMISSIONS UNIT INFORMATION

<u>Title V Air Operation Permit Emissions Unit Classification</u>

1.	or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)					
	□ The emissions unit addressed in this Emissions Unit Information Section is a regulated					
	emissions unit. The emissions unit addressed in this Emissions Unit Information Section is an					
	unregulated en					
En	nissions Unit Descr	ription and Status				
1.	Type of Emissions	Unit Addressed in this	Section: (Check one)			
	single process	s Unit Information Section or production unit, or ac which has at least one do	ctivity, which produces of	one or more air		
	of process or p	s Unit Information Section foroduction units and active vent) but may also produced	vities which has at least	e emissions unit, a group one definable emission		
		s Unit Information Section production units and a		e emissions unit, one or fugitive emissions only.		
2.	Description of Emi Two Fuel Tanks.	issions Unit Addressed i	n this Section:			
3.	Emissions Unit Ide	entification Number:				
4.	Emissions Unit	5. Commence	6. Initial Startup	7. Emissions Unit		
	Status Code:	Construction Date:	Date:	Major Group SIC Code:		
	A	2014	2016	49		
8.	Federal Program A	Applicability: (Check all	that apply)			
	☐ Acid Rain Unit	t				
	☐ CAIR Unit		_			
9.	Package Unit:					
	Manufacturer:		Model Number:			
	10. Generator Nameplate Rating: MW/CT					
11.	. Emissions Unit Co	mment:				

Section [3] FPL - Fuel Tanks

Emissions Unit Control Equipment/Method: Control of
1. Control Equipment/Method Description:
2. Control Device or Method Code:
Emissions Unit Control Equipment/Method: Control of
1. Control Equipment/Method Description:
2. Control Device or Method Code:
Emissions Unit Control Equipment/Method: Control of
1. Control Equipment/Method: Control of 1. Control Equipment/Method Description:
1. Control Equipment/Method Description:
1. Control Equipment/Method Description:
Control Equipment/Method Description: Control Device or Method Code:
Control Equipment/Method Description: Control Device or Method Code: Emissions Unit Control Equipment/Method: Control of
Control Equipment/Method Description: Control Device or Method Code: Emissions Unit Control Equipment/Method: Control of
Control Equipment/Method Description: Control Device or Method Code: Emissions Unit Control Equipment/Method: Control of

Section [3] FPL - Fuel Tanks

B. EMISSIONS UNIT CAPACITY INFORMATION

(Optional for unregulated emissions units.)

Emissions Unit Operating Capacity and Schedule

1.	Maximum Process or Throughp	out Rate: 40,816,197 gal	
2.	Maximum Production Rate:		
3.	Maximum Heat Input Rate:	million Btu/hr	
4.	Maximum Incineration Rate:	pounds/hr	
		tons/day	
5.	Requested Maximum Operating	Schedule:	
		24 hours/day	7 days/week
		52 weeks/year	8,760 hours/year
6.	Operating Capacity/Schedule Control Determined using maximum house operation.		i,918 lb/hour) and 500-hour
6.	Determined using maximum hou		i,918 lb/hour) and 500-hour
6.	Determined using maximum hou		i,918 lb/hour) and 500-hour
6.	Determined using maximum hou		i,918 lb/hour) and 500-hour
6.	Determined using maximum hou		i,918 lb/hour) and 500-hour
6.	Determined using maximum hou		i,918 lb/hour) and 500-hour
6.	Determined using maximum hou		i,918 lb/hour) and 500-hour

Section [3] FPL - Fuel Tanks

C. EMISSION POINT (STACK/VENT) INFORMATION

(Optional for unregulated emissions units.)

Emission Point Description and Type

1. Identification of Point on Flow Diagram:	Plot Plan or	2. Emission Point 7	Гуре Code:
3. Descriptions of Emission	Points Comprising	g this Emissions Unit	for VE Tracking:
			n i di G
4. ID Numbers or Description	ons of Emission Ui	nits with this Emission	
5. Discharge Type Code:	6. Stack Height feet	:	7. Exit Diameter: feet
8. Exit Temperature: °F	9. Actual Volur acfm	netric Flow Rate:	10. Water Vapor: %
11. Maximum Dry Standard F dscfm	low Rate:	12. Nonstack Emissi feet	ion Point Height:
13. Emission Point UTM Coo Zone: East (km): North (km)		14. Emission Point I Latitude (DD/M Longitude (DD/M	· · · · · · · · · · · · · · · · · · ·
15. Emission Point Comment: For each tank, Diameter = 114ft Height = 40ft Volume = 3,000,000 gal			

EMISSIONS UNIT INFORMATION Section [3] FPL - Fuel Tanks

D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment Description and Rate: Segment 1 of 1

	. Segment Description (Process/Fuel Type): Internal Combustion Engines; Electric Generation; Distillate Oil (Diesel); Turbine				
	ource Classification Code	e (SCC):	3. SCC Units: 1,000 Gallor		urned
4. N	Maximum Hourly Rate:	5. Maximum	Annual Rate:	6.	Estimated Annual Activity Factor:
1	Maximum % Sulfur: .0015	8. Maximum (% Ash:	9.	Million Btu per SCC Unit: 136
10. S	egment Comment:				
Segm	nent Description and Ra	te: Segment	of		
	egment Description (Proc				
		,			
2. S	ource Classification Code	e (SCC):	3. SCC Units:		
4. M	faximum Hourly Rate:	5. Maximum A	Annual Rate:	6.	Estimated Annual Activity Factor:
7. M	1aximum % Sulfur:	8. Maximum 9	% Ash:	9.	Million Btu per SCC Unit:
10. Se	egment Comment:				

Section [3] FPL - Fuel Tanks

E. EMISSIONS UNIT POLLUTANTS

List of Pollutants Emitted by Emissions Unit

	The state of the s			
1.	Pollutant Emitted	2. Primary Control	3. Secondary Control	4. Pollutant
		Device Code	Device Code	Regulatory Code
	VOC			EL
			-	
			_	
-				
		_	_	
-	-			
	_ .			

EMISSIONS UNIT INFORMATION Section [1] FPL - Fuel Tanks

POLLUTANT DETAIL INFORMATION
Page [1] of [1]
Volatile Organic Compounds

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Potential, Estimated Fugitive, and Baseline & Projected Actual Emissions

1 Otential, Estimated Fugitive, and Basenne of	110,00000 110	tuui Liiii	5310115
Pollutant Emitted: Volatile Organic Compounds - VOC	2. Total Perc	ent Efficie	ency of Control:
3. Potential Emissions:		4. Synth	netically Limited?
4.28 lb/hour 1.07	tons/year	□ Y	es 🛛 No
5. Range of Estimated Fugitive Emissions (as	s applicable):		
to tons/year			
6. Emission Factor:			7. Emissions
D. C			Method Code:
Reference:			
8.a. Baseline Actual Emissions (if required):	8.b. Baseline	24-month	Period:
tons/year	From:	T	o:
9.a. Projected Actual Emissions (if required):	9.b. Projected	l Monitori	ng Period:
tons/year		rs 🔲 10) years
Calculated using TANKs model. Total fuel storage volume is determined usin (115,918 lb/hour) and 500-hour operation. 115,918 lb/hr /(7.1 lb/gal) x 5 CTs x 500 hrs/yr Turnover is calculated using the total fuel sto 40,816,197 gal/yr / (2 x 3,000,000 gal) =7 /yr for Assuming white color for the roof and shell of the color for the color for the roof and shell of the color for the color for the roof and shell of the color for	e = 40,816,197 g orage volume a or each tank. of the tanks.	al/yr	

POLLUTANT DETAIL INFORMATION Page [1] of [1] Volatile Organic Compounds

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 1 of 1

1.	Basis for Allowable Emissions Code: OTHER	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: 4.28 lb/hour 1.07 tons/year
5.	Method of Compliance:		
6.	Allowable Emissions Comment (Description	of (Operating Method):
<u>Al</u>	lowable Emissions Allowable Emissions	<u> </u>	f
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:		
6.	Allowable Emissions Comment (Description	of (Operating Method):
_ <u>Al</u>	lowable Emissions Allowable Emissions	0	f
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:	•	
6.	Allowable Emissions Comment (Description	of (Operating Method):

EMISSIONS UNIT INFORMATION Section [3] FPL - Fuel Tanks

G. VISIBLE EMISSIONS INFORMATION

Complete Subsection G if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

<u>Vi</u>	sible Emissions Limitation: Visible En	nissio	ons Limitation of	
1.	Visible Emissions Subtype:		2. Basis for Allowable Opac ☐ Rule ☐ □	ity: Other
3.	Allowable Opacity: Normal Conditions: % Maximum Period of Excess Opacity Al		ceptional Conditions: d:	% min/hour
4.	•			
5.	Visible Emissions Comment:			
Vi	sible Emissions Limitation: Visible En	nissio	ons Limitation of	
_	sible Emissions Limitation: Visible En	nissio	2. Basis for Allowable Opac	ity:
1.	<u> </u>	Exc	2. Basis for Allowable Opac Rule Ceptional Conditions:	
3.	Visible Emissions Subtype: Allowable Opacity: Normal Conditions: %	Exc	2. Basis for Allowable Opac Rule Ceptional Conditions:	Other %

EMISSIONS UNIT INFORMATION Section [1] FPL - Fuel Tanks

H. CONTINUOUS MONITOR INFORMATION

Complete Subsection H if this emissions unit is or would be subject to continuous monitoring.

<u>Co</u>	ntinuous Monitoring System: Continuous	Mon	itor of
1.	Parameter Code:	2.	Pollutant(s):
3.	CMS Requirement:		Rule
4.	Monitor Information Manufacturer:		
	Model Number:		Serial Number:
5.	Installation Date:	6.	Performance Specification Test Date:
7.	Continuous Monitor Comment:		
Co	entinuous Monitoring System: Continuous	Mon	itor of
_	Parameter Code:		Pollutant(s):
_	Parameter Code: CMS Requirement:	2.	
1.	Parameter Code: CMS Requirement: Monitor Information Manufacturer:	2.	Pollutant(s): Rule
3. 4.	Parameter Code: CMS Requirement: Monitor Information Manufacturer: Model Number:	2.	Pollutant(s): Rule
1. 3.	Parameter Code: CMS Requirement: Monitor Information Manufacturer:	2.	Pollutant(s): Rule

EMISSIONS UNIT INFORMATION Section [1] FPL - Fuel Tanks

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated 1. Process Flow Diagram: (Required for all permit applications, except Title Vair

1.	revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: See Air Reports Previously Submitted, Date
2.	Fuel Analysis or Specification: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: See Air Reports Previously Submitted, Date
3.	Detailed Description of Control Equipment: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: See Air Reports Previously Submitted, Date
4.	Procedures for Startup and Shutdown: (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Previously Submitted, Date Not Applicable (construction application)
5.	Operation and Maintenance Plan: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Previously Submitted, Date Not Applicable
6.	Compliance Demonstration Reports/Records: Attached, Document ID: Test Date(s)/Pollutant(s) Tested:
	☐ Previously Submitted, Date: Test Date(s)/Pollutant(s) Tested: ☐ To be Submitted, Date (if known): Test Date(s)/Pollutant(s) Tested:
	Not Applicable Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute: Attached, Document ID: Not Applicable

Section [1] FPL - Fuel Tanks

I. EMISSIONS UNIT ADDITIONAL INFORMATION (CONTINUED)

Additional Requirements for Air Construction Permit Applications

1.	1. Control Technology Review and Analysis (Rules 62-212.400(10) and 62-212.500(7),				
	F.A.C.; 40 CFR 63.43(d) and (e)):				
2.	Good Engineering Practice Stack Height Analysis (Rules 62-212.400(4)(d) and 62-				
	212.500(4)(f), F.A.C.):				
	☐ Attached, Document ID: Not Applicable				
3.	Description of Stack Sampling Facilities: (Required for proposed new stack sampling facilities only)				
	☐ Attached, Document ID: ⊠ Not Applicable				
<u>A</u>	Iditional Requirements for Title V Air Operation Permit Applications				
1.	Identification of Applicable Requirements: Attached, Document ID:				
2.	Compliance Assurance Monitoring: Attached, Document ID: Not Applicable				
3.	Alternative Methods of Operation:				
4.	Alternative Modes of Operation (Emissions Trading): Attached, Document ID: Not Applicable				
Ad	Iditional Requirements Comment				

Section [4] **Diesel Fire Pump Engine**

Effective: 03/11/2010

III. EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Application - For Title V air operation permitting only, emissions units are classified as regulated, unregulated, or insignificant. If this is an application for an initial, revised or renewal Title V air operation permit, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each regulated and unregulated emissions unit addressed in this application. Some of the subsections comprising the Emissions Unit Information Section of the form are optional for unregulated emissions units. Each such subsection is appropriately marked. Insignificant emissions units are required to be listed at Section II, Subsection C.

Air Construction Permit or FESOP Application - For air construction permitting or federally enforceable state air operation permitting, emissions units are classified as either subject to air permitting or exempt from air permitting. The concept of an "unregulated emissions unit" does not apply. If this is an application for an air construction permit or FESOP, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air permitting are required to be listed at Section II, Subsection C.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit Application - Where this application is used to apply for both an air construction permit and a revised or renewal Title V air operation permit, each emissions unit is classified as either subject to air permitting or exempt from air permitting for air construction permitting purposes, and as regulated, unregulated, or insignificant for Title V air operation permitting purposes. A separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit addressed in this application that is subject to air construction permitting and for each such emissions unit that is a regulated or unregulated unit for purposes of Title V permitting. (An emissions unit may be exempt from air construction permitting but still be classified as an unregulated unit for Title V purposes.) Emissions units classified as insignificant for Title V purposes are required to be listed at Section II, Subsection C.

If submitting the application form in hard copy, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application must be indicated in the space provided at the top of each page.

> 14 07/2013

Section [4] Diesel Fire Pump Engine

A. GENERAL EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Emissions Unit Classification

11.	Emissions Unit Co One diesel fire pur determined (TBD).	mment: np engine rated at 300	hp.	Manufacturer and	model number to be	
10.	Generator Namepla	ate Rating: MW				
9.	Package Unit: Manufacturer: TBI	D		Model Number:	TBD	
	☐ Acid Rain Unit☐ CAIR Unit					
8.	_	applicability: (Check all	tha	t apply)		
4.	Emissions Unit Status Code:	5. Commence Construction Date: 2014	6.	Initial Startup Date:	7. Emissions Unit Major Group SIC Code: 49	
3.	Emissions Unit Ide	entification Number: 6				
2.	•	issions Unit Addressed in Ingine for emergency usa		iis Section:		
	☐ This Emissions	s Unit Information Secti	on a	iddresses, as a singl	e emissions unit, one or fugitive emissions only.	
	of process or p		vitie	es which has at least	e emissions unit, a group t one definable emission	
1.	 Type of Emissions Unit Addressed in this Section: (Check one) This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent). 					
<u>En</u>	nissions Unit Desci					
	 The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit. The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit. 					
1.	or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)					

Section [4] Diesel Fire Pump Engine

Emissions Unit Control Equipment/Method: Control 1 of 1

1.	Control Equipment/Method Description: Good combustion practices - No. 2 fuel oil-fired.
	Good Combustion practices - No. 2 fuel on-fired.
2.	Control Device or Method Code: N/A
En	nissions Unit Control Equipment/Method: Control of
1.	Control Equipment/Method Description:
2.	Control Device or Method Code:
En	nissions Unit Control Equipment/Method: Control of
1.	Control Equipment/Method Description:
2.	Control Device or Method Code:
Em	nissions Unit Control Equipment/Method: Control of
1.	Control Equipment/Method Description:
2.	Control Device or Method Code:

Section [4] Diesel Fire Pump Engine

B. EMISSIONS UNIT CAPACITY INFORMATION

(Optional for unregulated emissions units.)

Emissions Unit Operating Capacity and Schedule

1 March D TI 1		
 Maximum Process or Throughp 	out Rate:	
2. Maximum Production Rate:		
3. Maximum Heat Input Rate: 2.3	32 million Btu/hr	· .
4. Maximum Incineration Rate:	pounds/hr	
	tons/day	
5. Requested Maximum Operating	g Schedule:	
	24 hours/day	7 days/week
	52 weeks/year	100 hours/year
and maintenance. The fire pu Subpart IIII.		Phours per month for testing requirements of 40 CFR 60

Section [4] Diesel Fire Pump Engine

C. EMISSION POINT (STACK/VENT) INFORMATION

(Optional for unregulated emissions units.)

Emission Point Description and Type

1.	Identification of Point on Flow Diagram:	Plot Plan or	2. Emission Poi	nt Type Code:
3.	Descriptions of Emission ID Numbers or Descriptio			
5.	Discharge Type Code: V	6. Stack Height 17 feet	:	7. Exit Diameter: 0.8 Feet
8.	Exit Temperature: 744°F	9. Actual Volur 1,750 acfm	netric Flow Rate:	10. Water Vapor: %
11.	Maximum Dry Standard F dscfm	low Rate:	12. Nonstack Em Feet	ission Point Height:
13.	Emission Point UTM Coo Zone: East (km): North (km)		14. Emission Poi Latitude (DD Longitude (D	
15.	Emission Point Comment: See Table 2-7 in Air Permit		rt.	

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D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment Description and Rate: Segment 1 of 1

1.	1. Segment Description (Process/Fuel Type): Diesel fuel combustion					
2.	Source Classification Cod	e (SCC):	3. SCC Units 1,000 gallor			
4.	Maximum Hourly Rate: 0.017	5. Maximum 1.72	Annual Rate:	6.	Estimated Annual Activity Factor:	
7.	Maximum % Sulfur: 0.0015	8. Maximum	% Ash:	9.	Million Btu per SCC Unit: 137.7	
10.	Segment Comment: Maximum annual rate base	ed on 100 hr/yr op	peration.			
Sec	gment Description and Ra	ete: Segment	of			
	Segment Description (Pro-					
	-	• •				
2.	Source Classification Cod	e (SCC)·	3. SCC Units:			
2.	Source Classification Cod	,		•		
4.	Maximum Hourly Rate:	5. Maximum	Annual Rate:	6.	Estimated Annual Activity Factor:	
7.	Maximum % Sulfur:	8. Maximum % Ash:		9.	Million Btu per SCC Unit:	
10.	Segment Comment:			<u> </u>		

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Effective: 03/11/2010

EMISSIONS UNIT INFORMATION Section [4]

Section [4] Diesel Fire Pump Engine

E. EMISSIONS UNIT POLLUTANTS

List of Pollutants Emitted by Emissions Unit

1.	Pollutant Emitted	2. Primary Control Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
	СО			EL
	PM/PM10			EL
	NOX			EL
	SO2	Fuel Quality		EL
	VOC			EL
	,			
			_	
	_		_	

POLLUTANT DETAIL INFORMATION
Page [1] of [5]
Carbon Monoxide - CO

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Potential, Estimated Fugitive, and Baseline & Projected Actual Emissions

I Otennai, Estimated Fugitive, and Dasenne o	t i i o jected i ic	tuui Liiiis	SIGHS
Pollutant Emitted: Carbon Monoxide - CO	2. Total Perc	ent Efficie	ency of Control:
3. Potential Emissions:		_	netically Limited?
1.7 lb/hour 0.09	tons/year	⊠ Y	es 🗌 No
5. Range of Estimated Fugitive Emissions (as	applicable):		
to tons/year			
6. Emission Factor: 2.6 grams per horsepower	-hour (g/hp-hr)	-	7. Emissions
D 6			Method Code:
Reference: Manufacturer certification			2
8.a. Baseline Actual Emissions (if required):	8.b. Baseline	24-month	Period:
tons/year	From:	T	0:
9.a. Projected Actual Emissions (if required):	9.b. Projected	Monitori	ng Period:
tons/year	☐ 5 yea	rs 🔲 10) years
10. Calculation of Emissions:			
2.6 g/hp-hr x 300 hp x 1 lb/453.6 g = 1.7 lb/hr 1.7 lb/hr x 100 hr/2,000 lb = 0.09 TPY			
11. Potential, Fugitive, and Actual Emissions Co Emissions are for one engine.	omment:		

POLLUTANT DETAIL INFORMATION Page [1] of [5] Carbon Monoxide - CO

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 1 of 1

1.	Basis for Allowable Emissions Code: RULE	2. Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions:	
	2.6 g/hp-hr	1.7 lb/hour 0.09 tons/year	
5.	Method of Compliance: Manufacturer certification of Subpart IIII stand	dards.	
6.	6. Allowable Emissions Comment (Description of Operating Method):		
Al	lowable Emissions Allowable Emissions	of	
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions:	
		lb/hour tons/year	
	5. Method of Compliance:6. Allowable Emissions Comment (Description of Operating Method):		
Al	lowable Emissions Allowable Emissions	of	
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year	
5.	Method of Compliance:		
6.	Allowable Emissions Comment (Description	of Operating Method):	

POLLUTANT DETAIL INFORMATION
Page [2] of [5]
Nitrogen Oxides - NOX

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Potential, Estimated Fugitive, and Baseline & Projected Actual Emissions

	110 00000 110		
Pollutant Emitted: Nitrogen Oxides - NOX	2. Total Perc	ent Efficie	ency of Control:
3. Potential Emissions:		4. Synth	netically Limited?
	3 tons/year	⊠ Y	es 🗌 No
5. Range of Estimated Fugitive Emissions (as	s applicable):		
to tons/year			
6. Emission Factor: 6.8 g/hp-hr			7. Emissions
			Method Code:
Reference: Manufacturer certification			2
8.a. Baseline Actual Emissions (if required):	8.b. Baseline	24-month	Period:
tons/year	From:	T	o:
9.a. Projected Actual Emissions (if required):	9.b. Projected	l Monitori	ng Period:
tons/year	☐ 5 yea	rs 🗌 10) years
10. Calculation of Emissions: 6.8 g/hp-hr x 300 hp x 1 lb/453.6 g = 4.5 lb/hr 4.5 lb/hr x 100 hr x ton/2,000 lb = 0.23 TPY 11. Potential, Fugitive, and Actual Emissions Co	omment:		
Emissions are for one engine.	omment:		

POLLUTANT DETAIL INFORMATION Page [2] of [5] Nitrogen Oxides - NOX

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 1 of 1

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Emissions:	f Allowable
3.	Allowable Emissions and Units: 6.8 g/hp-hr	4.	Equivalent Allowable E 4.5 lb/hour	missions: 0.23 tons/year
5.	Method of Compliance: Manufacturer certification of Subpart IIII stand	dard	s.	
6.	6. Allowable Emissions Comment (Description of Operating Method):			
Al	lowable Emissions Allowable Emissions	(of	
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Emissions:	f Allowable
3.	Allowable Emissions and Units:	4.	Equivalent Allowable E lb/hour	missions: tons/year
5.	Method of Compliance:			
6.	Allowable Emissions Comment (Description	of	Operating Method):	
All	owable Emissions Allowable Emissions	(of	
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Emissions:	Allowable
3.	Allowable Emissions and Units:	4.	Equivalent Allowable E lb/hour	missions: tons/year
5.	Method of Compliance:	•		
6.	Allowable Emissions Comment (Description	of	Operating Method):	

POLLUTANT DETAIL INFORMATION
Page [3] of [5]
Sulfur Dioxide - SO2

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Potential, Estimated Fugitive, and Baseline & Projected Actual Emissions

Pollutant Emitted: Sulfur Dioxide - SO2	2. Total Perc	ent Efficie	ency of Control:
3. Potential Emissions: 0.004 lb/hour 0.0002	2 tons/year	4. Synth	netically Limited?
5. Range of Estimated Fugitive Emissions (as to tons/year	s applicable):		
6. Emission Factor: 0.0015% S fuel oil Reference: FPL, 2011			7. Emissions Method Code: 2
8.a. Baseline Actual Emissions (if required):	8.b. Baseline	24-month	Period:
tons/year	From:		o:
9.a. Projected Actual Emissions (if required):	9.b. Projected	Monitori	ng Period:
tons/year	☐ 5 year	rs 🗌 10) years
10. Calculation of Emissions: 0.0015% S x 64/32 (MW SO2/S) x 7.06 lb/gal x 16.9 gal/hr = 0.004 lb/hr 0.004 lb/hr x 100 hr x ton/2,000 lb = 0.0002 TPY			
11. Potential, Fugitive, and Actual Emissions Comment: Emissions are for one engine.			

POLLUTANT DETAIL INFORMATION Page [3] of [5] Sulfur Dioxide - SO2

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 1 of 1

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 0.0015% S fuel oil	4. Equivalent Allowable Emissions: 0.004 lb/hour 0.0002 tons/year
5.	Method of Compliance: Fuel vendor information	
	Allowable Emissions Comment (Description	
	owable Emissions Allowable Emissions	
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:	
6.	Allowable Emissions Comment (Description	of Operating Method):
Al	owable Emissions Allowable Emissions	of
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:	
6.	Allowable Emissions Comment (Description	of Operating Method):

POLLUTANT DETAIL INFORMATION
Page [4] of [5]
Particulate Matter - PM/PM10

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Potential, Estimated Fugitive, and Baseline & Projected Actual Emissions

		•
tons/year	4. Synth	netically Limited? es
applicable):	•	
		7. Emissions Method Code: 2
8.b. Baseline From:		Period: o:
· ·		ng Period:) years
mment:		
•	applicable): 8.b. Baseline From: 9.b. Projected	applicable): 8.b. Baseline 24-month From: T 9.b. Projected Monitori

POLLUTANT DETAIL INFORMATION
Page [4] of [5]
Particulate Matter - PM/PM10

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 1 of 1

$\overline{}$	<u> </u>			
1.	Basis for Allowable Emissions Code: OTHER	2.	Future Effective Date Emissions:	of Allowable
3.	Allowable Emissions and Units:	4.	Equivalent Allowable	Emissions:
	0.4 g/hp-hr		0.26 lb/hour	0.013 tons/year
5.	Method of Compliance: Manufacturer certification of Subpart IIII Stan	dard	s.	
6.	Allowable Emissions Comment (Description	of	Operating Method):	
Al	lowable Emissions Allowable Emissions	c	f	
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date Emissions:	of Allowable
3.	Allowable Emissions and Units:	4.	Equivalent Allowable	Emissions:
			lb/hour	tons/year
5.	Method of Compliance:			
6.	Allowable Emissions Comment (Description	of (Operating Method):	
All	lowable Emissions Allowable Emissions		f	
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date 6 Emissions:	of Allowable
3.	Allowable Emissions and Units:	4.	Equivalent Allowable lb/hour	Emissions: tons/year
5.	Method of Compliance:		_	
6.	Allowable Emissions Comment (Description	of (Operating Method):	

POLLUTANT DETAIL INFORMATION
Page [5] of [5]
Volatile Organic Compounds - VOC

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL, FUGITIVE, AND ACTUAL EMISSIONS

(Optional for unregulated emissions units.)

Complete a Subsection F1 for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V operation permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Potential, Estimated Fugitive, and Baseline & Projected Actual Emissions

Totential, Estimated Tugitive, and Dasenne d	110 00000 110		<u> </u>
Pollutant Emitted: Volatile Organic Compounds - VOC	2. Total Perc	ent Efficie	ency of Control:
3. Potential Emissions:		4. Synth	netically Limited?
	tons/year	⊠ Y	es 🗌 No
5. Range of Estimated Fugitive Emissions (as	applicable):		
to tons/year			
6. Emission Factor: 1.0 g/hp-hr			7. Emissions
			Method Code:
Reference: Manufacturer certification			2
8.a. Baseline Actual Emissions (if required):	8.b. Baseline	24-month	Period:
tons/year	From:	T	0:
9.a. Projected Actual Emissions (if required):	9.b. Projected	l Monitori	ng Period:
tons/year	☐ 5 yea	rs 🗌 10) years
10. Calculation of Emissions: 1.0 g/hp-hr x 300 hp x 1 lb/453.6 g = 0.66 lb/hr 0.66 lb/hr x 100 hr/2,000 lb = 0.033 TPY 11. Potential, Fugitive, and Actual Emissions Communication are for one engine.			
Emissions are for one engine.			

POLLUTANT DETAIL INFORMATION
Page [5] of [5]
Volatile Organic Compounds - VOC

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete Subsection F2 if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 1 of 1

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units: 1.0 g/hp-hr	4.	Equivalent Allowable Emissions: 0.66 lb/hour 0.033 tons/year	
5.	Method of Compliance: Manufacturer certification of Subpart IIII Standard	dard	is.	
6.	6. Allowable Emissions Comment (Description of Operating Method):			
<u>Al</u>	lowable Emissions Allowable Emissions	(of	
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year	
	5. Method of Compliance:			
6.	6. Allowable Emissions Comment (Description of Operating Method):			
Al	lowable Emissions Allowable Emissions	0	of	
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year	
5.	Method of Compliance:			
6.	Allowable Emissions Comment (Description	of (Operating Method):	

G. VISIBLE EMISSIONS INFORMATION

Complete Subsection G if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

Visible Emissions Limitation: Visible Emissions Limitation 1 of 1

<u> </u>	Sibic Emissions Emitation.	ons Emiliation 1 of 1	
1.	Visible Emissions Subtype: VE20	2. Basis for Allowable Op ☐ Rule	oacity: Other
3.	Allowable Opacity:		
	Normal Conditions: 20 % Ex	ceptional Conditions:	100 %
	Maximum Period of Excess Opacity Allowe	ed:	60 min/hour
4.	Method of Compliance: EPA Method 9		-
5.	Visible Emissions Comment: FDEP Rule 62-296.320(4)(b)1, F.A.C. requires provided by Rule 62-210.700.	20 percent opacity. Excess	emissions
Vis	sible Emissions Limitation: Visible Emissi	ons Limitation of	
1.	Visible Emissions Subtype:	2. Basis for Allowable Op ☐ Rule ☐	oacity: Other
3.	Allowable Opacity:		
	Normal Conditions: % Ex	ceptional Conditions:	%
	Maximum Period of Excess Opacity Allowe	ed:	min/hour
4.	Method of Compliance:		
5.	Visible Emissions Comment:		

H. CONTINUOUS MONITOR INFORMATION

Complete Subsection H if this emissions unit is or would be subject to continuous monitoring.

<u>Co</u>	ontinuous Monitoring System: Continuous	Monitor of
1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	☐ Rule ☐ Other
4.	Monitor Information Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
Co	ontinuous Monitoring System: Continuous	Monitor of
1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	☐ Rule ☐ Other
4.	Monitor Information Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	•

Effective: 03/11/2010

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: See Air Report Previously Submitted, Date		
2.	Fuel Analysis or Specification: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: See Air Report Previously Submitted, Date		
3.	Detailed Description of Control Equipment: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: See Air Report Previously Submitted, Date		
4.	Procedures for Startup and Shutdown: (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) ☐ Attached, Document ID: ☐ Previously Submitted, Date ☐ ☐ Not Applicable (construction application)		
5.	Operation and Maintenance Plan: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) ☐ Attached, Document ID: ☐ Previously Submitted, Date ☐ Not Applicable		
6.	Compliance Demonstration Reports/Records: Attached, Document ID: Test Date(s)/Pollutant(s) Tested:		
	☐ Previously Submitted, Date: Test Date(s)/Pollutant(s) Tested: ☐ To be Submitted, Date (if known):		
	Test Date(s)/Pollutant(s) Tested: Not Applicable Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.		
7.	Other Information Required by Rule or Statute: Attached, Document ID: See Air Report Not Applicable		

Section [4] Diesel Fire Pump Engine

Effective: 03/11/2010

I. EMISSIONS UNIT ADDITIONAL INFORMATION (CONTINUED)

Additional Requirements for Air Construction Permit Applications

1.	1. Control Technology Review and Analysis (Rules 62-212.400(10) and 62-212.500(7),		
	F.A.C.; 40 CFR 63.43(d) and (e)):		
		☐ Not Applicable	
2.	2. Good Engineering Practice Stack Height Analysis (Rules 62-212.400(4)(d) and 62-		
	212.500(4)(f), F.A.C.):		
	☐ Attached, Document ID:	☑ Not Applicable	
3.	 Description of Stack Sampling Facilities: (Required for proposed new stack sampling facilities only) 		
	Attached, Document ID:	☑ Not Applicable	
Additional Requirements for Title V Air Operation Permit Applications			
1.	Identification of Applicable Requirements: ☐ Attached, Document ID:		
2.	Compliance Assurance Monitoring: Attached, Document ID:	☐ Not Applicable	
3.	Alternative Methods of Operation: Attached, Document ID:	☐ Not Applicable	
4.	Alternative Modes of Operation (Emissions T Attached, Document ID:	rading): □ Not Applicable	
Additional Requirements Comment			
Additional Requirements Comment			