

November 15, 1995

Mr. Clair H. Fancy Bureau of Air Regulation Florida Department of Environmental Regulation 2600 Blair Stone Road, MS 5505 Tallahassee, FL 32399-2400.

Re: University of Florida Cogeneration Facility - Alachua County AC01-204652 and PSD-FL-181 Request to Amend Construction Permit

Dear Clair:

This correspondence is submitted to provide information requested in the Department's letter dated May 22, 1995, concerning Florida Power Corporation's (FPC's) request to amend the air construction and prevention of significant deterioration (PSD) permit application for the University of Florida cogeneration facility.

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The Department's responses to FPC's request to the custom fuel monitoring schedule and Specific Condition No. 2 are acceptable. At this time, the Department's response to FPC's request to amend Specific Condition No. 3 is acknowledged. FPC still has considerable concerns regarding the issue of simultaneous testing and may pursue alternative(s) to accommodate our concerns as suggested in the Department's response.

Specific Condition No. 8

The Department's response cited that portion of the BACT determination that indicated PSD review for NO_x was not required by assuring that a significant net emissions increase did not occur for the project. The "netting out" of PSD is appropriate under the Department's rules in Chapter 62-212 F.A.C. It must be recognized, however, that the criterion for PSD review is based on whether the project had a significant net emissions increase as defined in Rule 62-212.500(2)(e)2, F.A.C. The emissions rates for determining a significant net emission increase are in tons/year and were regulated in the permit based on annual fuel usage (refer to Specific Condition No. 3 of the permit).

As discussed in FPC's request to amend the permit, the increase in heat input and maximum NO_x emissions is for an operating condition that would occur only for short durations. This condition occurs at a turbine inlet temperature of 45°F. The manufacturer's curve for fuel use as a function of turbine inlet temperature is attached. This manufacturer's curve was developed from data supplied by General Electric Company and adjusted for actual machine performance. As can be seen from this graph, the maximum heat input and emissions occur at 45°F. The actual performance during the initial compliance test is also presented on the graph. The actual heat input during the test was 97 percent of the maximum heat input for the turbine inlet temperature that was measured during the test [i.e., actual of 344.6 x 10^3 standard cubic feet (kscf)/hr versus a maximum of 355 kscf].

Mr. Clair H. Fancy November 15, 1995 Page 2

To determine compliance with the lb/hr and ton/yr limits, the control system accounts for hourly and cumulative NO_x emissions using the following equation:

 NO_x (lb/hr) = 8.47830 - 17.33488 x SF Ratio + 0.00014 x FF

where: SF Ratio = Steam-to-Fuel Ratio FF = Fuel Flow (kscf)

This equation was developed using multiple regression analysis and had an R-squared value of 0.98709. This R-squared value indicates that over 98 percent of the variability in the NO_x emissions is accounted for in this equation. The ideal R-squared value is 1.0. The equation will be used until the CEM is installed and certified as required under 40 CFR Part 75.

Please call me at (813) 866-5158 if you should have any questions.

Sincerely,

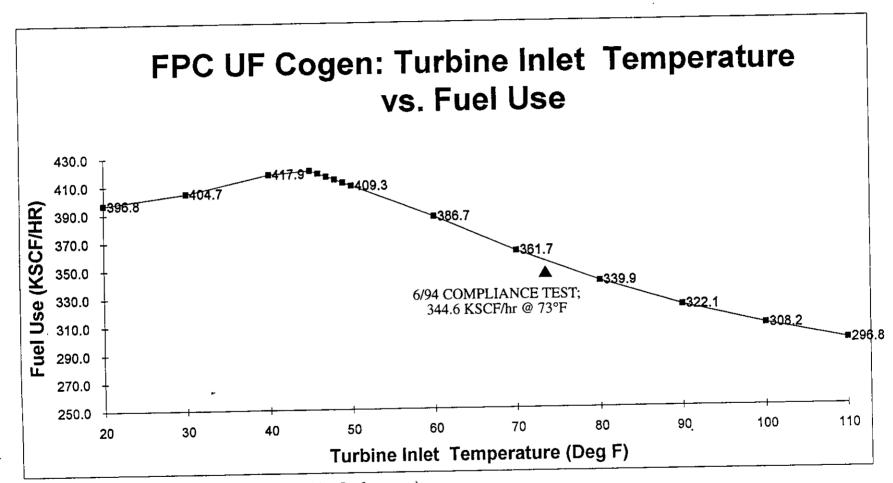
Scott H. Osbourn

Senior Environmental Engineer

Attachment

cc: Martin Costello, FDEP Kennard Kosky, KBN

Robert Leetch, FDEP NE District



(Manufacturer Curves - Adjusted for Actual Machine Performance)



Department of **Environmental Protection**

Lawton Chiles Governor

Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Virginia B. Wetherell Secretary

September 13, 1995

CERTIFIED MAIL - RETURN RECEIPT REQUESTED

Mr. Scott H. Osbourn Senior Environmental Engineer Florida Power Corporation 3201 Thirty-fourth Street South St. Petersburg, Florida 33733

Re: Extension of Permits No. AC 01-204652, University of Florida Cogeneration Facility AC 49-203114, Intercession City Facility

Dear Mr. Osbourn:

On August 30 the Department received your application letters, dated August 25. requesting an extension of the expiration date of the above referenced permits. The attached proposed rule language will, if adopted, extend the air construction permit by law. It is anticipated that the rule will be adopted in early September. If the rule is adopted within 90 days of receipt of your application, the Department will not be required to respond further. However, we will inform you upon adoption of the proposed rule.

If the rule, for any reason, is not adopted within 90 days of receipt of your application we will act upon your request in a timely manner. Please note that your air construction permit is valid until the Department acts upon your request.

Should you have any questions please contact me at (904) 488-1344.

Sincerely,

A. A. Linero, P.E.

Administrator, New Source Review

Section

AAL/kw

CC:

C. Collins, CD

E. Frey, NED

P. Reynolds, NED GBO

K. Kosky, KBN

NOTICE OF CHANGE IN PROPOSED RULE

DEPARTMENT OF ENVIRONMENTAL PROTECTION

DOCKET NO: 95-38R

CHAPTER TITLE:

CHAPTER NO.:

Operation Permits for Major Sources of Air

Pollution

62-213

RULE TITLE:

RULE NO.:

Permit Applications

62-213.420

The Department has made a change to the proposed rule which appeared in the Florida Administrative Weekly, Volume 21, Number 30, dated July 28, 1995, page 4958, so that the following section(s) will read as set forth below:

62-213.420 Permit Applications

- (1)(a)1.a. Acid Rain Sources will submit applications for the entire source by <u>June 15, 1996 January 1, 1996</u>. <u>The Acid Rain Part of each such application, however, shall be submitted no later than January 1, 1996</u>.
 - b.(ii) June 15, 1996 February 1, 1996, otherwise.
- c. All other sources subject to the permitting requirements of this chapter will submit applications by <u>June 15, 1996</u> February $\frac{1}{17}$ 1996.
- 2. Except as provided at Rule 62-213.420(1)(a)4., F.A.C., except for sources that are subject to the Florida Electrical Power Plant Siting Act (FEPPSA), a source that commences operation after January 1, 1996, must file an application for an operation permit under this chapter ninety days before expiration of the source's construction permit, but no later than 180 days after commencing operation. Except as provided at Rule 62-213.420(1)(a)4., F.A.C., aA source that has applied for an Electrical Power Plant Siting Certification prior to January 1, 1996, but has not but has not been issued the certification as of that date, or a source that has been issued an Electrical Power Plant Siting Certification prior to January 1, 1996, but has not commenced operation by that date, shall file an application for an operation permit under this conapter no later than 180 days after commencing operation. Sources subject to the FEPPSA that apply for Electrical Power Plant Siting Certification subsequent to January 1, 1996, may, at their option, shall apply for a permit under the provisions of this chapter at the same time the Florida Power Plant Siting Certification application is submitted.
- 4. The expiration dates of all air construction permits for Title V sources that expire between September 1, 1995, and November 1, 1996 September 1, 1996, are hereby extended to the later of November 1, 1996, or 240 days after commencing operation September 1, 1996. Facilities with such air construction permits which have not commenced operation on January 1, 1996, shall apply

for a permit under the provisions of this chapter on the later of September 1, 1996, or 180 days after commencing operation. Specific Authority: 403.061, 403.087, F.S. Law Implemented: 403.061, 403.0872, F.S. History: New 11-28-93; Amended 4-62-94; Formerly 17-213.420; Amended 11-23-94, 4-2-95,

NAME OF PERSON ORIGINATING PROPOSED RULE: Howard L. Rhodes, Director, Division of Air Resources Management NAME OF SUPERVISOR OR PERSON WHO APPROVED THE PROPOSED RULE: Virginia B. Wetherell, Secretary DATE PROPOSED RULE APPROVED: July 17, 1995

on the reverse side	SENDER: • Complete items 1 and/or 2 for additional services. • Complete items 3, and 4a & b. • Print your name and address on the reverse of this form so the return this card to you. • Attach this form to the front of the mailpiece, or on the back i does not permit. • Write "Return Receipt Requested" on the mailpiece below the article The Return Receipt will show to whom the article was delivered additivered.	I also wish to receive the following services (for an extra fee): 1. Addressee's Address 2. Restricted Delivery Consult postmaster for fee.	eceipt Service.	
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AUG 30 1995

Bureau of Air. Regulation

August 25, 1995

Mr. Al Linero
Bureau of Air Regulation
Florida Department of Environmental Protection
2600 Blair Stone Road
Tallahassee, Florida 32399-2400

Re:

Florida Power Corporation

University of Florida Cogeneration Facility
Permit Extension to Accommodate Title V

Dear Mr. Linero:

Due to the extensions of time for submitting Title V applications and the modification request we have under review, the above-referenced facility construction permit (AC 01-204652) and backup boiler operating permits (AO 01-214826, -214829, -214829, -214830, and -214831) require an extension to accommodate the Title V application due date. The Title V permit application for this source is currently due on January 1, 1996, and DEP has indicated that the application submittal deadline may be extended further, until June 15, 1996. As a consequence, an extension of the construction and operating permits referenced above till September 15, 1996 is requested. An extension till September 15, 1996 will allow for any future delays in the Title V application due dates.

If you should have any questions concerning the above, please feel free to contact me at (813) 866-5158.

Sincerely,

Scott H. Osbourn

Senior Environmental Engineer

cc:

Clair Fancy, FDEP

Ernest Frey, FDEP NE District

Patricia Reynolds, FDEP NE District GBO

Ken Kosky, KBN



Department of Environmental Protection

file

Lawton Chiles Governor Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Virginia B. Wetherell Secretary

May 22, 1995

CERTIFIED MAIL - RETURN RECEIPT REQUESTED

Mr. W. Jeffrey Pardue, Director Environmental Service Department Florida Power Corporation P. O. Box 14042 St. Petersburg, Florida 33733

Dear Mr. Pardue:

RE: University of Florida Cogeneration Facility Alachua County AC01-204652 and PSD-Fl-181

Request for Amendment of Construction Permit

The Department is in receipt of your March 31 letter requesting to incorporate the EPA approved custom fuel monitoring schedule and to amend Specific Conditions No. 2, No. 3, and No. 8 of the above mentioned permit. This permit was issued under a stipulated settlement (OGC case No. 91-1113). The Department has evaluated your request and determines the following:

CUSTOM FUEL MONITORING SCHEDULE:

FPC'S REQUEST:

To incorporate the EPA approved custom fuel monitoring schedule for sulfur in natural gas.

DEPARTMENT'S RESPONSE:

The Department will amend the permit to incorporate the fuel monitoring schedule. The attached EPA custom fuel monitoring schedule shall be part of this permit.

SPECIFIC CONDITION NO.2

FPC'S REQUEST:

To delete reference to boiler No. 2 with no increases in the current cap for typ of ${\rm NO}_{\rm X}$ for boilers No. 4 and 5.

"Protect, Conserve and Manage Florida's Environment and Natural Resources"

Mr. W. Jeffrey Pardue May 22, 1995 Page Two

DEPARTMENT'S RESPONSE:

Based on discussion with Company personnel, we understand FPC will withdraw this request and will use a rental boiler and the emergency order if needed. The Department's Office of General Counsel will review the draft order.

SPECIFIC CONDITION No.3

FPC'S REQUEST:

An Alternate to the NSPS testing requirements for the Subpart Db duct burner was proposed which involved combining the NO_X emission limits from the turbine and the duct burner. You provided a draft letter from the Department to EPA which proposed to demonstrate compliance with the duct burner NSPS NO_X emission standards (0.2 lb/MMBtu) without conducting a Method 20 upstream of the duct burner.

DEPARTMENT'S RESPONSE:

- o Subpart Db establishes NO_X emission limits for the gas fired duct burner (0.2 lb/MMBtu pursuant to 40 CFR 60.44b) and Method 20 is specified upstream and down stream of the duct burner to demonstrate compliance (40 CFR 60.46b).
- o 40 CFR 60.8(e)(1) requires the owner or operator of an affected facility to provide or cause to be provided, performance testing facilities including sampling ports adequate for test methods applicable to such facility.
- o The requested alternate testing procedure must be reviewed pursuant to Rule 62-297.620, F.A.C., Exceptions and Approval of Alternate Procedures and Requirements (attached). FPC should provide the information required in Rule 62-297.620, F.A.C.
- o The Department intends to deny the request to combine the emission limits from the turbine and duct burner unless and until an approved alternate sampling procedure is obtained from the Department's Emissions Monitoring Section. These are separate NSPS emissions units (Subpart GG and Subpart Db) and current NSPS regulations require that compliance be demonstrated for each emissions unit. The draft letter to EPA will not be sent. We understand that a second (revised) draft letter to EPA will be sent by FPC to the Department for review.

Mr. W. Jeffrey Pardue May 22, 1995 Page Three

The Department intends to amend ACO1-203652/PSD-FL-181 to require NO_X and CO testing prior to obtaining the operating permit. Compliance testing on the duct burner will not be required annually since this emissions unit emits less than 100 tpy of NO_X or CO and there are significant difficulties with conducting the required Method 20 upstream of the duct burner. This will allow additional time for FPC to resolve the duct burner compliance test issues.

SPECIFIC CONDITION No. 8

FPC'S REOUEST:

To increase heat input rate from the turbine by 10% and corresponding increases in lb/hr of NO_X with no increases in tpy. FPC indicated that tpy NO_X limits would be demonstrated using the water-to-fuel monitor until 1996 when a NO_X CEMS would be used in place of the water/fuel monitor. The NO_X CEMS will be installed to meet the requirements of 40 CFR Part 75.

DEPARTMENT'S RESPONSE:

The revised BACT determination for PSD-FL-181 established BACT for CO only. NO_X was not triggered for PSD review. There were 134.9 tpy of NO_X offsets listed from shutting down units 1, 2, and 3. The net increase in emissions totaled 39.7 tpy, just 0.3 tpy below the significance level for PSD review. From that BACT determination:

"The application indicates that emissions of other pollutants will not be subject to a BACT determination. The applicant narrowly escaped PSD review for NO_X by lowering firing rates, and since increased firing rates may be requested at some time in the future, the Department will require that retrofit costs associated with the applicant's decision not to make initial provisions for future installation of advanced catalytic control shall not be considered in any cost analysis required for any future requested increase in capacity".

- O BACT for similar combustion turbines when PSD-FL-181 was under review was 15 ppmvd @ 15% oxygen for gas firing to be obtained by 1997 or 1998. These emission levels were thought to be achievable using dry low NO $_{\rm X}$ combustor technology or SCR. This BACT, 15 ppmvd @ 15% oxygen, has been demonstrated currently using dry low NO $_{\rm X}$ burners. The NO $_{\rm X}$ standard in PSD-FL-181 was set at 25 ppmvd @ 15% oxygen for natural gas.
- o The requested increase in lb/hr of $NO_{\rm X}$ emissions constitutes a modification. If approved, the Department would reissue the construction permit and public notice this action.

Mr. W. Jeffrey Pardue May 22, 1995 Page Four

The following information is requested to help the Department resolve this request. Please describe how FPC determined that increased heat rates, and corresponding increased NO $_{\rm X}$ emission rates, are achievable based on the initial performance test. Provide manufactures curves and example calculations. Please describe how tpy of NO $_{\rm X}$ are monitored for each emissions unit. State if any F factors will be used when the NO $_{\rm X}$ CEMS system is used for NO $_{\rm X}$ tpy monitoring. Supply example calculations and state all assumptions for these calculations. Describe fuel and process monitoring associated with the NO $_{\rm X}$ monitoring.

Submit any written inquiries or additional information to me at the above address. If you have any questions or need clarification on any of these items, please call Martin Costello at (904)488-1344.

Sincerely,

C. H. Fancy P.

Chief

Bureau of Air Regulation

CHF/mc/h

attachments: Mr. Pardue's letter of March 31, 1995

EPA's custom fuel monitoring schedule guidance

Rule 62-297.620, F.A.C.

cc: Robert Leetch, NED

John Reynolds
Mike Harley
Morton Benjamin
Martin Costello

- 62-297.620 Exceptions and Approval of Alternate Procedures and Requirements.
- (1) The owner or operator of any emissions unit subject to the provisions of this chapter may request in writing a determination by the Secretary or his/her designee that any requirement of this chapter (except for any continuous monitoring requirements) relating to emissions test procedures, methodology, equipment, or test facilities shall not apply to such emissions unit and shall request approval of an alternate procedures or requirements.
- (2) The request shall set forth the following information, at a minimum:
- (a) Specific emissions unit and permit number, if any, for which exception is requested.
- (b) The specific provision(s) of this chapter from which an exception is sought.
- (c) The basis for the exception, including but not limited to any hardship which would result from compliance with the provisions of this chapter.
- (d) The alternate procedure(s) or requirement(s) for which approval is sought and a demonstration that such alternate procedure(s) or requirement(s) shall be adequate to demonstrate compliance with applicable emission limiting standards contained in the rules of the Department or any permit issued pursuant to those rules.
- (3) The Secretary or his/her designee shall specify by order each alternate procedure or requirement approved for an individual emissions unit source in accordance with this section or shall issue an order denying the request for such approval. The Department's order shall be final agency action, reviewable in accordance with Section 120.57, Florida Statutes.
- (4) In the case of an emissions unit which has the potential to emit less than 100 tons per year of particulate matter and is equipped with a baghouse, the Secretary or the appropriate Director of District Management may waive any particulate matter compliance test requirements for such emissions unit specified in any otherwise applicable rule, and specify an alternative standard of 5% opacity. The waiver of compliance test requirements for a particulate emissions unit equipped with a baghouse, and the substitution of the visible emissions standard, shall be specified in the permit issued to the emissions unit.

If the Department has reason to believe that the particulate weight emission standard applicable to such an emissions unit is not being met, it shall require that compliance be demonstrated by the test method specified in the applicable rule. Specific Authority: 403.061, F.S. Law Implemented: 403.021, 403.031, 403.061, 403.087, F.S. History: Formerly 17-2.700(3); Amended 6-29-93; Formerly 17-297.620; Amended 11-23-94.

SENDER: Complete items 1 and/or 2 for additional services. Complete items 3, and 4a & b. Print your name and address on the reverse of this form so the return this card to you. Attach this form to the front of the mailpiece, or on the back does not permit. Write "Return Receipt Requested" on the mailpiece below the art the Return Receipt will show to whom the article was delivered a delivered.	if space 1. Addressee's Address
3. Article Addressed to: The W. Officer Pardue Director Echucionnental Service Dept. 3. Article Addressed to: The W. Officer Pardue Director 5. Jla. Power Corp. 6. P. D. Box 14042 54. Pete, F1 33733	4a. Article Number Z 3/1 -902 897 4b. Service Type Registered Insured Certified COD Express Mail Return Receipt for Merchandise 7. Date of Delivery MAY 3 0 1995
5. Signature (Agent) 6. Signature (Agent) PS Form 3811, December 1991 \$\pmu.s. GPO: 1993—35	8. Addressee's Address (Only if requested and fee is paid) 2-714 DOMESTIC RETURN RECEIPT

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March 31, 1995

Mr. Clair H. Fancy, P.E., Chief **Bureau of Air Regulation** Florida Department of Environmental Protection 2600 Blair Stone Road Tallahassee, FL 32399-2400



Dear Mr. Fancy:

Re: **UF Cogeneration Facility** ACO1-204652; PSD-FL-181; Alachua County Request for Amendment of Construction Permit

This correspondence and attached application are submitted to request some minor changes to the construction permit issued for the University of Florida (UF) Cogeneration Facility. The source is a nominal 43-megawatt (MW) cogeneration facility located adjacent to the University of Florida Central Heating Plant in Gainesville, Alachua County, Florida. The cogeneration facility consists of one combustion turbine (CT) exhausting through a heat recovery steam generator (HRSG). The primary fuel for the CT is natural gas with a maximum fuel input of 367.9 thousand cubic feet per hour (Mcf/hr). Distillate fuel oil is used for the CT only as backup. The transition duct from the CT to the HRSG was permitted with duct burners (DBs) having a maximum fuel (natural gas) input of 197.7 Mcf/hr.

The construction permit was issued August 17, 1992, and expires October 1, 1995. Initial compliance tests were performed on June 3 and 4, 1994, and test results indicate that compliance was demonstrated for all units. However, detailed review of these tests and an inspection of the facility revealed some areas where changes to permit conditions are necessary. Changes to Specific Conditions 2, 3 and 8 are requested. Please be advised, however, that this request for amendments does not constitute any change in total emissions from the facility. The initial tests for the facility demonstrated that the CT and DBs can achieve the basis of the nitrogen oxides (NO₂) emission limit. This is an extremely low emission rate given the energy efficiency of the CT.

Further, in response to New Source Performance Standard (NSPS) requirement 40 CFR 60.334(b), Florida Power Corporation (FPC) has requested a customized fuel monitoring schedule. The EPA has indicated concurrence with FPC's approach and the Department has indicated that this request would require a permit amendment. All pertinent correspondence on this issue from FPC, the Department and EPA Region IV is presented in Attachment 1 to this letter.

The following paragraphs present a discussion of the amendments requested for each of the specific conditions. Attachment 2 contains a mark-up of these conditions with the revisions requested.

Mr. Clair H. Fancy March 31, 1995 Page 2

Specific Condition 2

This condition sets forth the emission limits for the facility (see attached Specific Condition). As discussed in the construction permit application, the CT selected for this project is the most efficient of all CTs and is the newest aircraft-derivative CT available from General Electric (i.e., the LM 6000). Indeed, when the application was submitted, there were no operating data on this machine while achieving the performance and emission guarantees proposed for this project. The initial testing of the CT indicated several areas where performance has been higher than expected. The maximum fuel flow rate of the CT is slightly higher than that initially specified by the manufacturer (GE). Accordingly, an increase in the short-term [pounds per hour (lb/hr)] NOx emission rate for the CT to 39.6 lb/hr is requested based on a requested increase in heat input (see Specific Condition 3). The basis for the limit is still 25 parts per million by volume, dry (ppmvd) corrected to 15 percent 0₂.

Specific Condition 3

It is requested that the heat input be increased based on the performance tests. The maximum fuel usage rate to the turbine when firing natural gas in the current permit is 367.9 Mcf/hr. The maximum operating condition is at 45°F with a fuel input of 420.3 Mcf/hr and is based on GE data and the test results. During the compliance tests, the CT averaged 97 percent of the maximum heat input based on CT inlet temperature conditions. The requested maximum heat input corresponds to the maximum emission limit requested (See discussion for Specific Condition 2 above).

Specific Condition 8

It is requested that this condition be amended to delete the reference to boiler no. 2. FPC proposes to continue operation of boiler no. 2, which is equipped to fire natural gas as its primary fuel. FPC proposes that the same fuel use restrictions apply to this boiler as currently apply to boilers 4 and 5. Therefore, there would be no increase in emissions since the facility will demonstrate compliance with its annual emissions limits in tons per year.

Also, as a result of discussions between FPC and the Department, a draft Emergency Order has been prepared for the Department's review. This order would allow a back-up boiler to be used in an emergency (e.g., in the event that the cogeneration facility and the backup boilers become inoperable) in order to meet the steam demands required for the University of Florida and Shands Hospital.

Finally, a draft letter is enclosed regarding an alternative approach for demonstrating compliance with the NSPS for cogeneration or combined cycle systems with duct firing. This letter represents the understanding reached between FPC and the Department and is meant for the Department's use in obtaining concurrence from the EPA. Please contact Mr. Scott Osbourn if you should have any questions at (813) 866-5158. As always, your consideration in this matter is appreciated.

Sincerely,

W. Jeffrey Pardue, C.E.P.

Director, Environmental Services Department

Attachments

ATTACHMENT A



UNITED STATES ENVIRONMENTAL PROTECTION AGENCY

AUG 14 1227

AT MAKE OF

HZHORAHDUY

BUBJEOT: Authority for Approval of Custom Puel Honitoring

FROM: John B. Rasnic, Chief Cole Practice
Compliance Honizoring France

porter und teath artiful

TO: .. Air Compliance Branch Chicae Regions II, III, IV, V, VI and IX

Air Programs Branch Chiefe Regions I-X

The Keys for Stationary Das Turbinas (Subpart 66) at 40 CPR 60.134(B)(2) allows for the development of Surface fuel monitoring sonedules 45 an alternative to daily conitoring of the gultur and nitrogen concent of fuel fired in the furniture. Regional offices between the manuface compliance division (5500) for consideration since it was understood that summerity for approval of these consultation with the imission Standards and inginesting division, it has been determined that the Regional Offices do have the authority to approve suppart to outside fuel confideration have the authority to approve suppart to outside fuel confideration have the authority to approve suppart to outside fuel confideration and have the authority to approve suppart to outside fuel confideration of the confideration of th

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Where courses using oil request susten fuel menitoring perhadules, Regional Offices are encouraged to contact saco for consultation on the appropriate fuel menitoring schedule. However, Regions are not required to send the request iterate to deed for approval.

If you have any quartions, please contact saily H. Parkell at III 182-2618.

Atteachment

DDI John Gronohiy Goorge Wilch Robert Ajax EXIL SX10

TELL NOT

Conditions for Custom Fuel Sampling Schedule for Stationary Gls Turbing

- 1. Henitoring of fuel nitroyen content shall not be required while nat gas is the only fuel fired in the gas turbing.
- 2. Sulfur Monitoring
 - a. Analyzis for fuel sulfur content of the natural gas shall be conducted using one of the approved ASTK reference methods for the measurement of sulfur in gaseous fuels, or an approved alternative method. The reference methods are: ASTK D1072-80; ASTK D3031-81; ASTK D3246-81; and ASTK D4884-82 as referenced in 40 CFR 60.335(b)(2).
 - b. Effective the date of this custom reneouse, sulfur monitoring that he conducted twice menthly for six months. If this monitoring shows little variability in the fuel sulfur content. and indicates consistent compliance with 40 CFR 60.313, then sulfur monitoring shall be conducted once per quarter for six quarters.
 - c. If after the mentering required in item 2(b) above, or herein. The sulfur content of the fuel shows little variability and, calculated at sulfur dioxide, represents consistent compliance with the sulfur dioxide amission limits specified under 40 CFR 60.333, sample analysis shall be conducted twice per annum. This mentering shall be conducted during the first and third quarters of each calendar year.
 - d. Should any sulfur analysis as required in (tems 2(b) or 2(c) abindicate noncompliance with 40 CPR 50.313, the owner or operate shall notify the State Air Control Board) of such excess emissions and the custom schedule shall be re-examined by the Environmental Protection Agency. Sulfur monitoring shall be conducted weekly during the interim period when this custom schedule is being re-examined.
 - If there is a change in fuel supply, the owner or operator must notify the State of such change for re-examination of this custom schedule. A substantial change in fuel quality shall be considered as a change in fuel supply. Sulfur monitoring shall be conducted waskly during the interim period when this custom schedule is being re-examined.
 - A. Records of sample analysis and such supply persinent to this custom achedule shall be retained for a period of three years, and be evaluated for inspection by personnel of seconds, state, and local air pollucicontrol agencies.

March 23, 1995

Jewell A. Harper, Chief Air Enforcement Branch U.S. Environmental Protection Agency, Region IV 345 Courtland Street, N.E. Atlanta, GA 30365



Dear Ms. Harper:

RE: Demonstrating Compliance with NSPS

Combustion Turbines and Duct Burners

University of Florida Cogeneration Facility PSD-FL-181

The Florida Department of Environmental Protection (FDEP) has been approached by Florida Power Corporation (FPC), which owns and operates the University of Florida Cogeneration facility, regarding an alternative approach for demonstrating compliance with the NSPS for combined cycle systems with duct firing. The UF facility has a nominal 43 megawatt (MW) combustion turbine (CT) firing primarily natural gas that exhausts through a heat recovery steam generator (HRSG). In the transition duct between the CT and HRSG, there are duct burners (DB) with a maximum heat input capability greater than 100 million (MM) Btu/hr while firing only natural gas. An air construction/Prevention of Significant Deterioration (PSD) permit was issued in August, 1992 and the facility become operational in 1994. The only exhaust point is through a stack connected to the HRSG. The NSPS applicable to the UF facility include Subpart GG (for the combustion turbine) and Subpart Db (for the duct burners). The only pollutant at issue is NOx emissions. The NSPS for the combustion turbine is 75 parts per million volume-dry conditions (ppmvd) corrected to 15 percent oxygen and adjusted for heat rate; the NSPS for the duct burners is 0.2 lb/MMBtu heat input.

As you are aware, the UF facility like so many other cogeneration facilities that have been recently permitted in Florida, have emission limitations established that are substantially lower than NSPS levels. For example, the UF facility has a CT lb/hr emission limit based on 25 ppmvd corrected to 15 percent oxygen and a DB lb/hr limit based on 0.1 lb/MMBtu. The CT limit is about 5 times lower than the NSPS while the DB limit is one half of the NSPS.

In order to demonstrate compliance with the NSPS for this facility, there is an implied requirement in Subpart Db and Method 20 to perform simultaneous sampling of the turbine exhaust and the exhaust stack to determine compliance with NSPS. This requirement can be difficult, if not impossible to perform and introduce costly testing procedures. It is this Department's position that the simultaneous testing requirement is unnecessary and that the source should be presumed in compliance with the NSPS, if the source can demonstrate that its combined CT/DB NOx emissions using EPA Method 20 at the single exhaust stack are less than the emissions that would be allowed under either <u>Subpart GG or Db</u>. The following information obtained for the UF Cogeneration facility demonstrates this conclusion.

CT: the applicable NSPS under Subpart GG (i.e., 75 ppmvd @ 15% O_2 ; corrected for heat rate) during conditions of the initial compliance test would produce an emission rate of 92 lb/hr.

DB: the applicable NSPS under Subpart Db (i.e., 0.2 lb/MMBtu) during the conditions of the initial compliance test would produce an emission rate of 42 lb/hr (for 210.2 MMBtu/hr heat input).

March 23, 1995 Page Two

CT/DB: the combined NOx emissions during the initial compliance test were 29.3 lb/hr while both the CT and DB were operating. The CT NOx emissions were 21.6 ppmvd @ 15% 0_2 (ISO) and the DB emissions were 0.05 lb/MMBtu. The combined applicable NSPS would be 134 lb/hr.

As noted above, since the testing demonstrated, using Method 20, that the combined NOx emissions (i.e., 29.3 lb/hr) were less than either Subpart GG or Db emissions limits, compliance with the NSPS requirements should be considered met. Therefore, the implied requirement in Subpart Db and Method 20 to perform simultaneous sampling of the turbine exhaust and the exhaust stack to determine compliance with NSPS is not necessary.

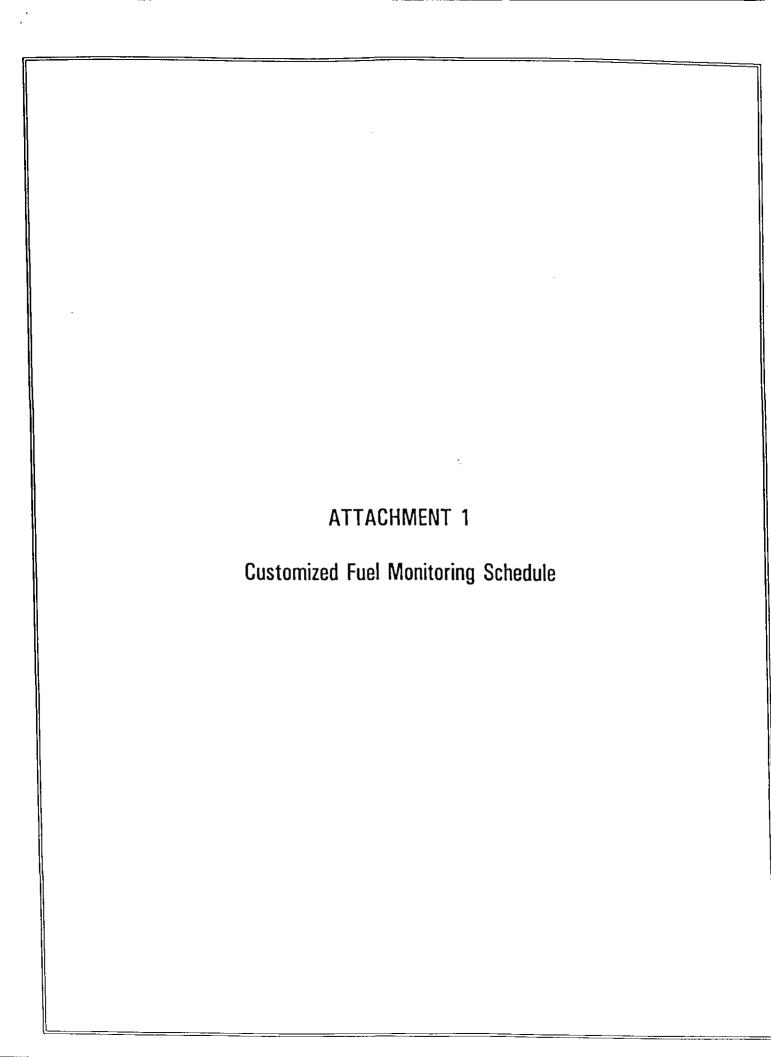
It is also the Department's position that if the combined CT/DB NOx emission limits established in the permit are met during annual compliance testing, the simultaneous testing to demonstrate continued compliance with NSPS would not be required for this source.

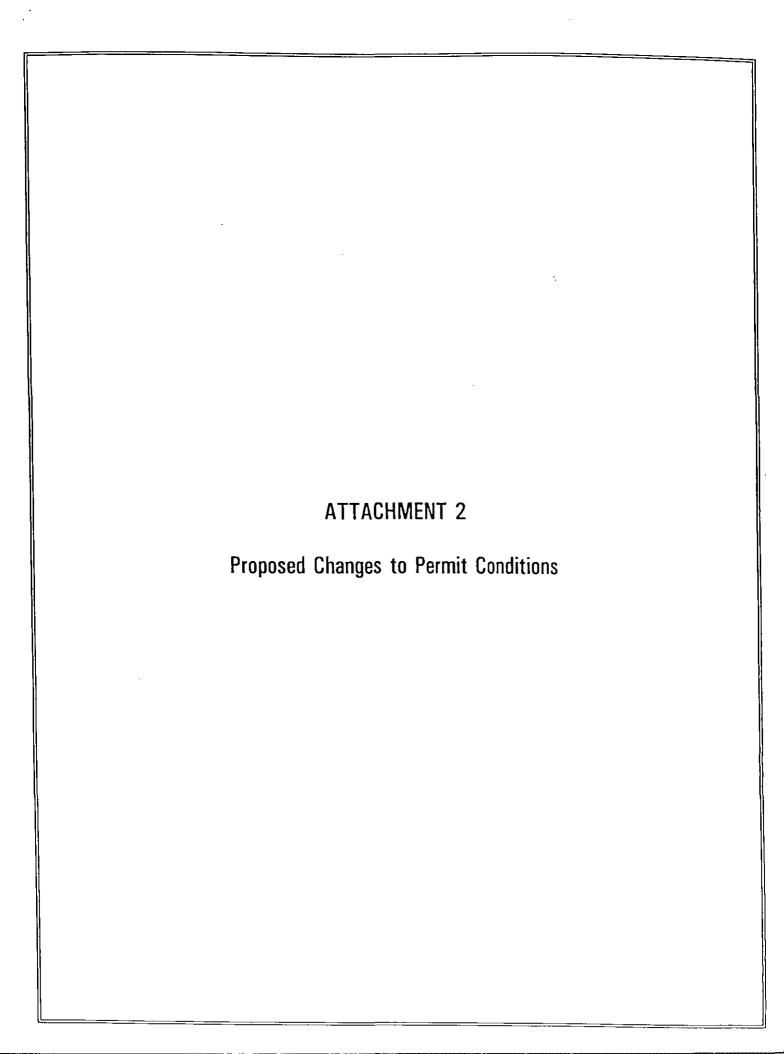
The Department would appreciate the Region's concurrence with this approach. A written response is respectfully required as this approach may apply to other cogeneration facilities and its implementation would assist the Department in evaluating compliance with these projects. Please call me at (904) 488-1344 if you have any questions.

Sincerely,

Clair H. Fancy, P.E., Chief Bureau of Air Regulation

cc: Scott Osbourn, FPC Ken Kosky, KBN John Reynolds, BAR Martin Costello, BAR Mort Benjamin, FDEP





PERMITTEE:

Florida Power Corporation

Permit Number: AC 01-204652

PSD-FL-181

Expiration Date: December 31, 1994

SPECIFIC CONDITIONS:

2. Emissions from this facility shall not exceed the limits listed below:

				Perposeu
Pollu-				CHANGES
tant	Source	Fuel	Basis of Limit	lbs/hr tons/yr
NOX	Turbine	Gas	EBH*:25 ppmvd @ 15% 02	35.0(39.4) 142.7
C, ~ ~	Turbine	Oil	EBH*:42 ppmvd @ 15% 02	66.3
TURBINE	D. Burner	Gas	EBH*: 0.1 1b/MMBTU FOR D.B.	24.6(167.3)
so2	Turbine (2)	Oil	BACT: 0.5% Sulfur Max.	- 4
	Boiler 4	Oil	BACT: 0.5% Sulfur Max.	_
وستدوي والمتا	Boiler 5	011	BACT: 0.5% Sulfur Max.	er of the control of
graphic to the first		A Property	(1) The control of th	State of the state
VE	Turbine 🔔	Gas/Oil	Equivalent of mass EBM*	10%/20% opacity**
	D. Burner 5;	Gas	94 W 94	10% opacity
	Boiler 4	Gas/Oil	14 es pc	10%/20% opacity**
	Boiler'5	Gas/O11	H N H	10%/20% opacity**
co	Turbine	Gas	BACT: 42 ppmvd	38.8 158.0
	Turbine	Oil	EBA***:75 ppmvd	70.5 ~~~~ 7.7 ~~
 	D.Burner_	Gas	BACT: 0.15 lb/MMBTU****	28-1-(66.9) 36.9(194.9)
¢EBM∗	Petabliched b	w manufa		

*EBM: Established by manufacturer

***EBA: Established by applicant

3. Fuel consumption rates and hours of operation for the turbine and duct burner shall not exceed those listed below:

CHANGE BROBOTED

	Natural Gas		No. 2 Fuel Oil			
H ft3/h	r* MM ft3/yr		M_gal/hr*			
Turbine (420.3) 367.9	2997.2**	8146.8**	2.9	635.1	219.0**	
Duct Burner 197.7	519.5	2628.0	0	О	0	

^{*}Based on maximum firing rates. Units may run at lower rates for more hours within annual fuel limits.

^{**}Except for one 6-minute period per hour of not more than 27% opacity

^{****}BACT limit proposed by applicant in Table A-2 of application For D. B. + TOTAL CONTRIBUTION FROM TURBINE And Duck BURNIA

^{**}An additional 1.9 hours/yr operation on natural gas will be allowed for each 1.0 hour/yr that fuel oil is not burned (up to 219 x 1.9 hours/yr), in which case, the emission limits in Specific Condition No. 2 shall be adjusted accordingly.

PERMITTEE:

Florida Power Corporation

Permit Number: AC 01-204652

PSD-FL-181

Expiration Date: December 31, 1994

SPECIFIC CONDITIONS:

If test results from the turbine and duct burner show that it is unlikely that NO_X limits can be met, a revised BACT determination for NO_X shall also be considered. The Department may revise the BACT determination to require installation of such technology if so indicated by the revised BACT cost/benefit analysis. If the permittee has elected not to provide for future addition of such technology in the initial construction and later applies for a permit modification to increase capacity, the retrofit costs associated with not making provisions for such technology (initially) shall not be considered by the Department in the retrofit cost analysis required for the future expansion.

- retrofit cost analysis required for the future expansion.

 8. Boilers Nos. 1, 2 and 3 shall permanently cease operation upon receipt of the operation permit for the cogeneration facility.
- 9. The permittee, for good cause, may request that this construction permit be extended. Such a request shall be submitted to the Bureau of Air Regulation prior to 60 days before the expiration of the permit (F.A.C. Rule 17-4.090).
- 10. An application for an operation permit must be submitted to the Northeast District office at least 90 days prior to the expiration date of this construction permit. To properly apply for an operation permit, the applicant shall submit the appropriate application form, fee, certification that construction was completed noting any deviations from the conditions in the construction permit, and compliance test reports as required by this permit (F.A.C. Rules 17-4.055 and 17-4.220).

Issued this 17th day of August , 1992

STATE OF FLORIDA DEPARTMENT OF ENVIRONMENTAL REGULATION

Carol M. Browner, Secretary

STATE OF FLORIDA DEPARTMENT OF ENVIRONMENTAL PROTECTION

ORDER

GRANTING TEMPORARY USE OF EMERGENCY BACKUP BOILER CAPABILITY TO MEET COMMITMENT FOR UNINTERRUPTIBLE STEAM DEMAND

Florida Power Corporation (FPC) having requested issuance of an order to permit use of an Emergency Backup Boiler at its University of Florida Cogeneration Site and the Department having been fully advised in the premises, the Secretary finds as follows:

FINDINGS OF FACT

- 1. FPC has a commitment to the University of Florida, including Shands Hospital, to provide an uninterruptible supply of steam.
- 2. In the unlikely event that the cogeneration facility and either Backup Boiler 4 or 5 (or both) become inoperable, an emergency backup steam supply source will be required. This is because Backup Boilers 4 and 5 are both necessary to provide replacement steam for loss of the cogeneration facility and cannot supply all steam potentially necessary if required to serve as backups for each other.

CONDITIONS OF USE OF EMERGENCY BACKUP BOILER

1. In accordance with the Florida Statutes, Chapter 120.59 pertaining to Orders, the Secretary is authorized to grant exceptions from air construction permits and can allow the use of an Emergency Backup Boiler in order that Florida Power Corporation (FPC) may meet its commitment for uninterruptible steam demand when the primary sources of steam supply are inoperable.

- 2. In the event that FPC is unable to meet steam demand to the University of Florida due to the inoperability of any of the primary sources of steam supply (i.e., the cogeneration facility and Backup Boilers 4 and 5), the Secretary authorizes FPC to operate an additional boiler as an Emergency Backup.
- 3. The use of such an Emergency Backup shall not result in an increase in permitted air emissions over the limits prescribed by the Department in Permit No. AC01-204652 (PSD-FL-181).

ORDER

Subject to the Conditions of Use	of Emergency	Backup Boiler	cited above, the
Secretary hereby grants approval to FPC	for use of an	Emergency Bac	kup Boiler at its
University of Florida Cogeneration site.	DONE AND	ENTERED THIS	6 day
of, 199, in Tallahassee, Florida.			

STATE OF FLORIDA DEPARTMENT OF ENVIRONMENTAL PROTECTION

VIRGINIA WETHERELL Secretary

Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32301 Telephone: (904) 488-4805

File: u\:UFORDER



Department of Environmental Protection

Lawton Chiles Governor Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Virginia B. Wetherell Secretary

December 5, 1994

CERTIFIED MAIL-RETURN RECEIPT REQUESTED

Mr. W. Jeffrey Pardue, C.E.P. Florida Power Corporation P. O. Box 14042 St. Petersburg, Florida 33733

RE: UF Cogeneration Project AC01-204652, PSD-FL-181 Request for Permit Amendment

Dear Mr. Pardue:

The Bureau of Air Regulation has reviewed the above referenced request and determined that it will require a new permit as discussed in the December 1 meeting. The customized fuel monitoring request can be processed separately, but the \$250 processing fee must be submitted as indicated in our letter dated May 11, 1994. If you have any questions, please call Patty Adams at (904)488-1344.

Sincerely,

C. H. Fancy, P.E.

Chief

Bureau of Air Regulation

CHF/pa

cc: John Reynolds

on the reverse side?	SENDER: Complete items 1 and/or 2 for additional services. Complete items 3, and 4a & b. Print your name and address on the reverse of this form so the return this card-to you. Attach this form to the front of the mailpiece, or on the back i does not permit. Write "Return Receipt Requested" on the mailpiece below the article The Return Receipt will show to whom the article was delivered a delivered.	f space cle number. nd the date	Consult postmaster for fee.
IN ADDRESS completed	3. Article Addressed to: Mr. W. Jeffrey Parude, C.E.P. Florida Power Corporation P. O. Box 14042 St. Petersburg, Florida 33733	₽ 8 4b. Ser ☐ Regis X Certi ☐ Expro	
your RETURN	6. Signature (Agent) PS Form 2011, December 1991 \$\(\pi\)u.S. GPO: 1992—323	and	Gee is paid) DMESTIC RETURN RECEIPT

P 872,562.687

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Sec	ir. W. Jeffrey Pardue	
	Box 14042	
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1	Mailed: 12/07/94 ACO1-204652, PSD-FL-181	
	8	



November 28, 1994

RECEIVED

Bureau of Air Regulation

Mr. Clair H. Fancy, P.E., Chief
Bureau of Air Regulation
Florida Department of Environmental Protection
2600 Blair Stone Road
Tallahassee, FL 32399-2400

Dear Mr. Fancy:

Re: UF Cogeneration Project

ACO1-204652; PSD-FL-181; Alachua County Request for Amendment of Construction Permit

This correspondence is submitted to request some minor changes to the construction permit issued for the University of Florida (UF) cogeneration facility. The source is a nominal 43-megawatt (MW) cogeneration facility located adjacent to the University of Florida Central Heating Plant in Gainesville, Alachua County, Florida. The cogeneration facility consists of one combustion turbine (CT) exhausting through a heat recovery steam generator (HRSG). The primary fuel for the CT is natural gas with a maximum fuel input of 367.9 thousand cubic feet per hour (Mcf/hr). Distillate fuel oil is used for the CT only as backup. The transition duct from the CT to the HRSG was permitted with duct burners (DBs) having a maximum fuel (natural gas) input of 197.7 Mcf/hr.

The construction permit was issued August 17, 1992, and expires December 31, 1994. Initial compliance tests were performed on June 3 and 4, 1994, and test results indicate that compliance was demonstrated for all units. However, detailed review of these tests and an inspection of the facility revealed some areas where changes to permit conditions are necessary. Changes to Specific Conditions 2, 3 and 8 are requested. Further, in response to New Source Performance Standard requirement 40 CFR 60.334(b), FPC has requested a customized fuel monitoring schedule. The EPA has indicated concurrence with FPC's approach and the Department has indicated that this request would require a permit amendment. All pertinent correspondence on this issue from FPC, the Department and EPA Region IV is presented in Attachment 1 to this letter.

Please be advised, however, that this request for amendments does not constitute any change in total emissions from the facility. The initial tests for the facility demonstrated that the CT and DBs can achieve the basis of the nitrogen oxides (NO_x) emission limit. This is an extremely low emission rate given the energy efficiency of the CT.

The following paragraphs present a discussion of the amendments requested for each of the specific conditions. Attachment 2 contains a mark-up of these conditions with the revisions requested.

Specific Condition 2

This condition sets forth the emission limits for the facility (see attached Specific Condition). As discussed in the construction permit application, the CT selected for this project is the most efficient of all CTs and is the newest aircraft-derivative CT available from General Electric (i.e., the LM 6000). Indeed, when the application was submitted, there were no operating data on this machine while achieving the performance and emission guarantees proposed for this project. The initial testing of the CT indicated several areas where performance has been higher than expected. The maximum fuel flow rate of the CT is slightly higher than that initially specified by the manufacturer (GE).

Based on the initial tests and final configuration of the facility, the following changes are requested.

- CT Emissions of NO₂ Increase short-term [pounds per hour (lb/hr]] CT emission rate to 39.6 lb/hr based on a requested increase in heat input (see discussion for Specific Condition 3). The basis for the limit is still 25 parts per million by volume, dry (ppmvd) corrected to 15 percent O₂.
- 2. Specify CT/DB Emission Limits It is requested that the Department consider changing the specification of individual limits for DBs to emission limits applicable to the CT/DBs operating together. As noted above, there will be no increase in annual emissions or in the basis upon which the hourly rate is determined (i.e., 0.1 lb/MMBtu) with this requested change to the permit. The reasons for this request are fourfold.

First, the large volume flow rate of the CT could produce erroneous results when trying to determine compliance with a DB only emissions limit. The combination of large flow rate and smaller emission contribution from the DBs can produce substantial apparent errors when none exist.

Secondly, determining the emission status of the facility will be much easier for both the operators and FDEP by having specific limits for the CT and CT/DB combination. Since the facility will install a continuous emission monitoring (CEM) system for NO_x , and this system will be reporting total NO_x downstream of both units, determining the emission status would be directly evident.

Third, the DBs cannot be operated without the CT; therefore, it is logical to specify emission limits for the combination rather than separately.

Finally, the original compliance testing was performed using simultaneous testing at the CT exhaust and the stack to determine compliance with NSPS Subpart Db requirements. Since the emissions from the DB were very low compared with the NSPS limit (i.e., 0.04 lb/MMBtu from the test compared with the NSPS limit of 0.2 lb/MMBtu) and there is no explicit applicable NSPS requirement to perform annual testing for NSPS purposes, a separate DB emission limit and implicit testing are unnecessary. If, for example, the emissions from the DB approached the NSPS limit, a combined limit would be exceeded. A combined limit would be 58.3 lb/hr; if the DB were at NSPS levels, then its contribution would be 64 percent of the total leaving only a 36 percent contribution from the CT. This is equivalent to a CT contribution of 20.9 lb/hr, which is not technically possible with steam injection. The combined limit also would demonstrate compliance with the basis of the BACT determination. Therefore, the emissions cannot exceed the original emission basis of 25 ppmvd at 15 percent O₂ for the CT and 0.1 pound per million British thermal units (lb/MMBtu) for the DBs.

Also, please note that many of the emission limits for the facility, including NO_x , were not established as BACT. Since the facility is replacing, to a large extent, the steam generated by the old University of Florida steam plant, emission offsets were credited to the new cogeneration plant, thus netting out of PSD review.

3. Emergency Steam Demands - The steam demands of the University of Florida necessitate that the facility, which includes Boilers 4 and 5, provide an uninterrupted steam supply. This uninterrupted steam is required for Shands Hospital. In the unlikely event that the cogeneration facility and Boilers 4 and/or 5 become inoperable, an emergency backup source is required. This is because Boilers 4 and 5 are both necessary to provide replacement steam for loss of the cogeneration facility (i.e., they are not backups for each other). It is requested that the permit allow provisions to accommodate this emergency backup condition. This could be accomplished by either allowing the continued operation of one of the three boilers currently scheduled for retirement or by allowing the use of a rented boiler, when needed. The same fuel use restrictions would apply to this boiler as Boilers 4 and 5; there would be no increase in emissions since the facility must demonstrate compliance with its annual emissions limits in tons per year.

Specific Condition 3

It is requested that the heat input be increased based on the performance tests. The maximum fuel usage rate to the turbine when firing natural gas in the current permit is 367.9 Mcf/hr. The maximum operating condition is at 45°F with a fuel input of 420.3 Mcf/hr and is based on GE data and the test results. During the compliance tests, the CT averaged 97 percent of the maximum heat input based on CT inlet temperature conditions. The requested maximum heat input corresponds to the maximum emission limit requested (See discussion for Specific Condition 2, Item 1 above).

Specific Condition 8

It is requested that this condition be amended to reflect continued operation of one of these three boilers, if necessary.

Please contact Mr. Scott Osbourn if you should have any questions, at (813) 866-5158. As always, your consideration in this matter is appreciated.

Sincerely.

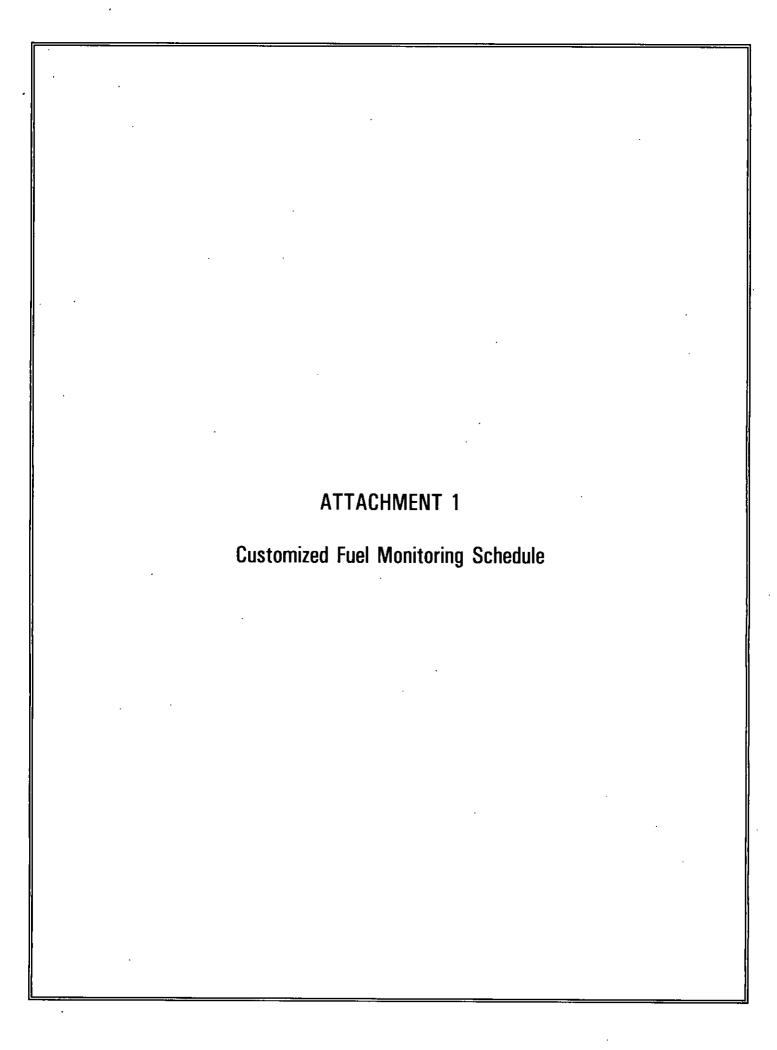
W. Jeffrey Pardue, C.E.P.

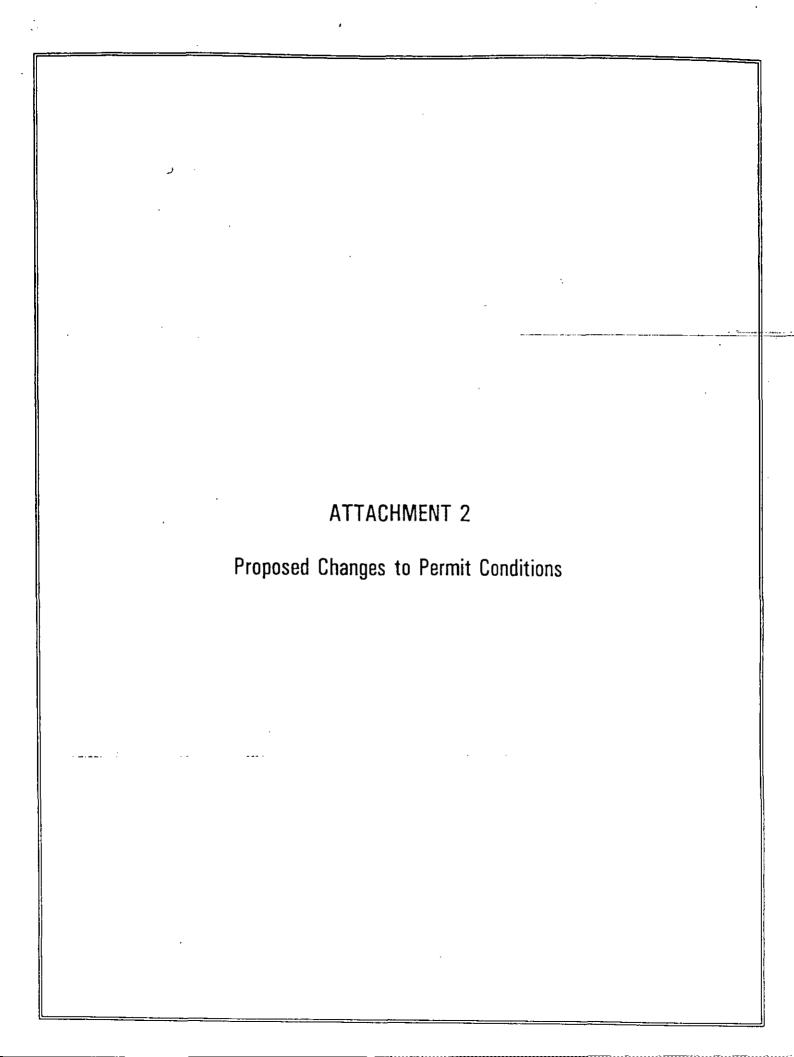
Director, Environmental Services Department

J. Michael Francy for

/mrb

Attachments





PERMITTEE:

Florida Power Corporation

AC 01-204652 Permit Number:

PSD-FL-181

Expiration Date: December 31, 1994

SPECIFIC CONDITIONS:

Emissions from this facility shall not exceed the limits listed below PROPOSED

						1	LHANGES
	Pollu- tant	Source	Fuel	Basis o	f Limit	lbs/hr	tons/yr
•	NOX	Turbine	Gas		mvd @ 15% O2	35.0/39.	
		Turbine	Oil		mvd @ 15% 02	66.3	7.3
(TVABINE	, , , , , ,	Gas (ombinite		D/HMBTU FOR D.B.	82) 81	
	502	Turbine Si) oil	71	Sulfur Max		=
		Boiler 4	Oil	BACT: 0.5%	Sulfur Max.	_	
		Boiler 5	011	BACT: 0.5%	Sulfur Max.		
···_·	1-1-			: -	1.00		• •
	VE	Turbine	Gas/Oil	Equivalent	of mass EBM*	10%/20%	opacity**
		D. Burner C	Gas	16	w H	10%	opacity
		Boller 4	Gas/OIL	**		10%/20%	opacity**
		Boller'5	Gas/Oil	80	n 14	10%/20%	opacity**
	co	Turbine	Gas	BACT: 42 p	pmvd 10 Lb/h-	38.8	158.0
_		Turbine	Oil	EBA***:75	ppmvd	70.5	7.7
		D.Burner	Gas		1b/MMBTU****	28-1- 66	ر 9.4 <u>9 (۹.۹) د د ده (۹.۹)</u>
		Datable about				~	

*EBM: Established by manufacturer

**Except for one 6-minute period per hour of not more than 27% opacity

***EBA: Established by applicant

****BACT limit proposed by applicant in Table A-2 of application For D. B. + TOTAL CONTRIBUTION FROM TUNBINE AND DUCK BYRNER

Fuel consumption rates and hours of operation for the turbine and duct burner shall not exceed those listed below:

PROPOSED CHANGE

~ = ·	Natural_Gas			No. 2 Fuel Oil		
W	H ft3/hr*	MM ft3/yr	hrs/yr*	M_gal/hr*	M gal/yr	hre/yr*
Turbine (420.3)	3 67:9	2997.2**	8146.8**	2.9	635.1	219.0**
Duct Burner	197.7	519.5	2628.0	0	0	0
	LaTestad @ zor MCF/h					

- *Based on maximum firing rates. Units may run at lower rates for more hours within annual fuel limits.
- **An additional 1.9 hours/yr operation on natural gas will be allowed for each 1.0 hour/yr that fuel oil is not burned (up to 219 x 1.9 hours/yr), in which case, the emission limits in Specific Condition No. 2 shall be adjusted accordingly.

210 mm DT Whr

Jos mm Btyhr

29 16/16 = 14 Lb/mmBTu

PERMITTEE: Florida Power Corporation

Permit Number: NC 01-204652

PSD-FL-181

Expiration Date: December 31, 1994

SPECIFIC CONDITIONS:

£

If test results from the turbine and duct burner show that it is unlikely that NO_X limits can be met, a revised BACT determination for NO_X shall also be considered. The Department may revise the BACT determination to require installation of such technology if so indicated by the revised BACT cost/benefit analysis. If the permittee has elected not to provide for future addition of such technology in the initial construction and later applies for a permit modification to increase capacity, the retrofit costs associated with not making provisions for such technology (initially) shall not be considered by the Department in the retrofit cost analysis required for the future expansion.

8. Boilers Nos. 1, 2 and 3 shall permanently cease operation upon receipt of the operation permit for the cogeneration facility.

9. The permittee, for good cause, may request that this construction permit be extended. Such a request shall be submitted to the Bureau of Air Regulation prior to 60 days before the expiration of the permit (F.A.C. Rule 17-4.090).

10. An application for an operation permit must be submitted to the Northeast District office at least 90 days prior to the expiration date of this construction permit. To properly apply for an operation permit, the applicant shall submit the appropriate application form, fee, certification that construction was completed noting any deviations from the conditions in the construction permit, and compliance test reports as required by this permit (F.A.C. Rules 17-4.055 and 17-4.220).

Issued this 17th day of August , 1992

STATE OF FLORIDA DEPARTMENT OF ENVIRONMENTAL REGULATION

Carol M. Browner, Secretary

David L. Miller Senior Vice President Corporate Services

October 21, 1994

TO WHOM IT MAY CONCERN

Subject: Letter of Authorization

Please be advised that W. Jeffrey Pardue, Director, Environmental Services Department, Sharon K. Momberg, Manager of Waste Management Programs, Kent D. Hedrick, Manager of Water Programs, J. Michael Kennedy, Manager of Air Programs, and Patricia Quets, Environmental Project Manager, are authorized to represent Florida Power Corporation in matters relating to necessary permits and reporting documentation required from regulatory authorities in the areas of air, water, power plant site certifications and transmission line certifications, or hazardous and solid materials issues.

Sincerely,

David L. Miller

DLM:bb



Department of **Environmental Protection**

Lawton Chiles Governor

Northeast District 7825 Baymeadows Way, Suite B200 lacksonville, Florida 32256-7590

Virginia B. Wetherell Secretary

CERTIFIED - RETURN RECEIPT

August 4, 1994

Mr. W. Jeffery Pardue, C.E.P. Florida Power Corporation P.O.Box 14042 (H2G)

St. Petersburg, Florida 33733

RECEIVED

AUG 1 5 1994

Environmental Svcs Department

Dear Mr. Pardue:

Alachua County - AP Florida Power Corp. at UF Emission Unit / Permit No. Cogen GT Plant / AC01-204652 / 31JAX01000101

This permit is extended to 06-02-95 to coordinate this emissions unit with the submittal of the Title V source (facility) permit application which shall be submitted by 04-02-95 per FAC Rule 17-213.420(1)(a)1.a.

Since this extension is in lieu of processing an operation permit application for a short-term operation permit, the testing required by this permit shall be performed initially and annually thereafter.

Any party to this Order (permit) has the right to seek judicial review of the permit pursuant to Section 120.68, Florida Statutes, by filing a Notice of Appeal pursuant to Rule 9.110, Florida Rules of Appellate Procedure, with the Clerk of the Department in the office of General Counsel, 2600 Blair Stone Road, Tallahassee, Florida 32399-2400; and by filing a copy of the Notice of Appeal accompanied by the applicable filing fees with the appropriate District Court of Appeal. The Notice of Appeal must be filed within 30 days from the date this Notice is filed with the Clerk of the Department.

If there are any questions, please contact Johnny Cole at (904) 448-4310, Ext. 236.

Ernesť E. Fréy, P.E.

FON Director of District Management

EEF:RU

"Protect, Conserve and Manage Florida's Environment and Natural Resources"

Printed on recycled paper.

Memorandum

Florida Department of **Environmental Protection**

TO:

Chris Kirts

FROM:

Mike Harley

DATE:

June 29, 1994

SUBJECT: Emission Test Report for Florida Power Corporation's Combined Cycle System at the University of Florida

The Emissions Monitoring Section received a copy of the test report for the compliance test of Florida Power Corporation's (FPC) combined cycle unit at the University of Florida. Martin Costello [Emissions Monitoring Section] was one of the Department representatives who witnessed the emission testing on Friday, June 3, 1994. We have reviewed the test report and note the following deviations:

- (1) The sampling site prior to the duct burner did not include a sufficient number of ports to permit sampling in accordance with EPA Method 20. This is a substantial deviation from EPA Method 20 requiring prior approval of an alternate sampling procedure pursuant to Rule 17-297.620, F.A.C. It is also a violation of 40 CFR 60.8(e).
- (2) The test runs at the sampling site prior to the duct burner were conducted with a multipoint probe which had a sealed end and holes drilled along the length of the probe. This is a substantial deviation from EPA Method 20 requiring prior approval of an alternate sampling procedure pursuant to Rule 17-297.620, F.A.C. EPA Method 20 requires the use of an open ended tube of sufficient length to traverse the sample points and the collection of an individual sample at each traverse point.
- (3) EPA Method 20 requires the collection of diluent samples at each traverse point for an equal period of time in order to identify any points where stratification may occur within the duct. EPA Method 20 then requires the collection of NOx samples for an equal period of time at the eight traverse points where the pollutant is least dilute. use of the multipoint probe and single sampling port did not permit sampling at each traverse point. Further, there is no assurance that an equal sample aliquot was collected at each of the sample points. Again this is a substantial deviation from EPA Method 20 requiring prior approval of an alternate sampling procedure pursuant to Rule 17-297.620. F.A.C.

TO: Chris Kirts DATE: June 29, 1994

PAGE: Two

An owner or operator who wishes to deviate from the applicable source testing requirements is required to file a formal request for approval of an alternate sampling procedure pursuant to Rule 17-297.620, F.A.C. The request should be submitted to the Division of Air Resources Management in Tallahassee and will be reviewed by the Emissions Monitoring Section. In the case of a source subject to the NSPS, the EPA would need to review and concur with the request before it could be approved. The required procedures remain in effect until the Department formally acts to approve the request.

It would be appropriate to reject the test results and consider an enforcement action for the 40 CFR 60.8(e) violation. A copy of a recent EPA letter concerning another combined cycle system is enclosed for your information. If you have any questions, please call me or Martin Costello (904) 488-1344.

cc: C. Fancy

J. Pennington

J. Brown

M. Benjamin



UNITED STATES ENVIRONMENTAL PROTECTION AGENCY

REGION IV

345 COURTLAND STREET, N.E. ATLANTA, GEORGIA 30365

.IIIN 1.5 1994

4APT-AEB

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JUN 2 1 1994

Environmental Sycs Department

Clair H. Fancy, P.E., Chief Bureau of Air Regulation Florida Department of Environmental Protection 2600 Blair Stone Road Tallahassee, FL 32399-2400

Re: Approval of NSPS Custom Fuel Monitoring Schedules for: Florida Power Corporation (FPC), University of Florida Cogeneration Project, PSD-FL-181

Dear Mr. Fancy:

This is to acknowledge a letter from Mr. Scott H. Osbourn of FPC dated April 5, 1994, requesting approval of customized fuel monitoring schedules for the above referenced project. This letter was addressed to you and a copy was sent to the U.S. Environmental Protection Agency (EPA). Since the authority for implementing \$60.334(b) of 40 CFR Part 60, Subpart GG has not been delegated to the State of Florida, we have reviewed FPC's custom fuel monitoring schedule.

Based on our review we have determined that the proposed schedule is acceptable, because it conforms to custom fuel monitoring quidance memo issued by EPA headquarters on August 14, 1987. A copy of this memo was included in FPC's request as attachment.

If you have any questions regarding this letter, please contact Mr. Mirza P. Baig of my staff at 404/347-5014.

Jewell A. Harper, Chief Air/Enforcement Branch Air/ Pesticides, & Toxics

Management Division

cc: Scott H. Osbourn, FPC



UNITED STATES ENVIRONMENTAL PROTECTION AGENCY

Pily file

REGION IV

345 COURTLAND STREET, N.E. ATLANTA, GEORGIA 30365

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4APT-AEB

Clair H. Fancy, P.E., Chief Bureau of Air Regulation Florida Department of Environmental Protection 2600 Blair Stone Road Tallahassee, FL 32399-2400 ANN S 0 1887

Bureau of Air. Regulation

Re: Approval of NSPS Custom Fuel Monitoring Schedules for: Florida Power Corporation (FPC), University of Florida Cogeneration Project, PSD-FL-181

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Sincerely yours,

Jewell A. Harper, Chief Air Enforcement Branch

Air, Pesticides, & Toxics

Management Division

cc: Scott H. Osbourn, FPC

RECEIVED

JUL 05 1994

Emissions Monitoring



Florida Department of **Environmental Protection**

Twin Towers Office Building 2600 Blair Stone Road -Tallahassee, Florida 32399-2400

Virginia B. Wetherell Secretary

May 11, 1994

CERTIFIED MAIL-RETURN RECEIPT REQUESTED

Mr. Scott H. Osbourn Senior Environmental Engineer Florida Power Corporation P. O. Box 14042 St. Petersburg, FL 33733

Dear Mr. Osbourn:

RE:

Florida Power Corporation University of Florida Cogeneration Project

AC 01-204652, PSD-FL-181

Customized Fuel Monitoring Schedule

The Bureau of Air Regulation has reviewed your April 5, 1994, letter concerning the above referenced request and determined that it will require a permit amendment. As soon as the processing fee of \$250 is received, we will begin processing your request. If you have any questions, please call Patty Adams at (904)488-1344.

Sincerely,

Bureau of Air Regulation

CHF/pa

SENDER: Complete items 1 and/or 2 for addition per Les E Complete items 3, and 4a & b. Print your name and address on the reverse of this form so the return this card to you. Attach this form to the front of the mailpiece, of the dackides not permit. Write "Return Receipt Requested" on the mailpiece below the article was delivered.	icle number. 2. Restricted Delivery Consult postmaster for fee.
Mr. Scott H. Osbourn Senior Environmental Engineer Florida Power Corporation P. O. Box 14042 St. Petersburg, Florida 33733	Article Number P 872 563 635 4b. Service Type Registered Insured XX Certified COD Express Mail Return Receipt for Merchandise 7. Date of Delivery MAY 1 6 1994
5. Signature (Addressee) 6. Signature (Agent) PS Form 3811, December 1990 & U.S. GPO: 1992—32:	8. Addresse's Address (Only if requested and fee is paid) 3-402 DOMESTIC RETURN RECEIPT

P 872 563 635

No.	Receipt for Certified Mail No Insurance Coverage Provided Do not use for International Mail (See Reverse)					
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April 5, 1994

Mr. C. H. Fancy, Chief Bureau of Air Permitting Department of Environmental Protection 2600 Blair Stone Road Tallahassee, FL 32399

Dear Mr. Fancy:

Re: Florida Power Corporation (FPC)
University of Florida Cogeneration Project
AC 01-204652; PSD-FL-181
Customized Fuel Monitoring Schedule

RECEIVED
APR 1 1 1994

Bureau of Air Regulation

The FPC University of Florida Cogeneration Project has been permitted under the above-referenced PSD permit. This unit consists of an advanced combustion turbine with a heat recovery steam generator (HRSG). The combustion turbine is subject to New Source Performance Standards (NSPS-40 CFR 60, Subpart GG). 40 CFR 60.334(b) requires the owner/operator of any combustion turbine to monitor the sulfur and nitrogen content of the fuel as follows: 1) If the turbine fuel is supplied by a bulk storage tank, then the sulfur and nitrogen content are to be determined whenever new fuel is transferred into the bulk storage tank, and 2) If the turbine fuel is supplied without an intermediate bulk storage tank then daily monitoring of the sulfur and nitrogen content of the fuel is required.

Since the natural gas used by the combustion turbine does not pass through an intermediate bulk storage tank, FPC is hereby requesting a customized fuel monitoring schedule as allowed by 40 CFR 60.334(b)(2). While firing natural gas, FPC requests the following customized fuel monitoring schedule which was developed based on an EPA guidance memorandum (Attachment A):

- Monitoring of natural gas nitrogen content shall not be required in accordance with page 2 of the EPA guidance memorandum attached.
- 2. Sulfur Monitoring
 - a. Analysis for sulfur content of the natural gas shall be conducted using one of the EPA approved ASTM reference methods for the measurement of sulfur in gaseous fuels, or an approved alternate method. The reference methods are: ASTM D1072-80; ASTM D3031-81; ASTM D3245-81; and ASTM D4048-82 as referenced in 40 CFR 60.335(b)(2).

- b. Effective on the approval date of the customized fuel monitoring schedule, sulfur monitoring shall be conducted twice a month for six months. If this monitoring shows little variability in the sulfur content and indicates consistent compliance with 40 CFR 60.333, then sulfur monitoring shall be conducted once per quarter for six quarters.
- c. If the monitoring required by 2(b), above, of the sulfur content of the natural gas shows little variability and the calculated sulfur dioxide emissions represent consistent compliance with the sulfur dioxide emission limits specified under 40 CFR 60.333, sample analysis shall be conducted twice per year. This monitoring shall be conducted during the first and third quarters of each calendar year.
- d. Should any sulfur analysis as required by items 2(b) or 2(c) above indicate noncompliance with 40 CFR 60.333, FPC will notify the Department of Environmental Protection of such excess emission and the customized fuel monitoring schedule shall be reexamined. The sulfur content of the natural gas will be monitored weekly during the interim period while this monitoring schedule is being reexamined.
- 3. FPC will notify the Department of Environmental Protection of any change in natural gas supply for reexamination of this monitoring schedule. A substantial change in natural gas quality (i.e., sulfur content varying greater than 10 grains/1000 cf gas) shall be considered as a change in natural gas supply. Sulfur content of the natural gas will be monitored weekly during the interim period when this monitoring schedule is being reexamined.
- 4. Records of sampling analysis and natural gas supply pertinent to this monitoring schedule shall be retained by FPC for a period of three years, and be available for inspection by appropriate regulatory personnel.
- FPC will obtain the sulfur content of the natural gas from Florida Gas Transmission Company at its Brooker Lab.

Data from natural gas at the Brooker Lab site is considered representative of the sulfur content of the natural gas at the University of Florida site since there is no additional entry point for sulfur or other elements/compounds which may affect the quality of the natural gas.

If you or your staff have any questions about this request, please call me at (813) 866-5158.

Sincerely,

Scott H. Osbourn

Senior Environmental Engineer

Attachments

cc/attach: Mike Harley, FDEP

David McNeal, Region IV, EPA 9. Rumoldo 9. Cale, NE West

APPENDIX A

ATTACHMENT A



United States Environmental Protection agency WASHINGTON, D.C. 20460

AUG 14 1327

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SUBJECTS

Authority for Approval of Custon Fiel Konitoring

Schadulas Under HSPS Suppart GO

FRONT

John B. Resnie, Chief Coppliance Monitoring Manon

101

Air Compliance Branch Chiefa Regions II, III, IV, V, VI and IX

Air Programs Branch Chiefe Regions I-X

The MEPS for Stationary Gas Turbines (Subpart 66) at 40 CPR 60.334(b)(2) allows for the development of custom fuel menitoring edhedules 48 an alternative to daily monitoring of the guldur and nitrogen content of fuel fired in the turbines. Regional officas have been forwarding euctom fuel monitoring schodules to the Stationary Source Compliance Division (SSCD) for consideration since it was understood that sutherity for approval of these consideration with the Emission Standards and Engineering Division, it has been determined that the Regional Offices do have the Euchority to approve Subpart to outlon fuel Fondoring canodules. Sherefore is it no longer necessary to serverd these requests to Headquarters for approval.

Gver the past few years, ESCD has issued over twenty queton activations for sources using pipeline quality natural que. In order to maintain national consistency, we recommend that any schodules Regional Offices issue for natural que be no loca attingent than the fullowing: sulfur sonitoring should

2

be blackthly, followed by quartarly, then certainfuel, given at least six months of data demonstrating little variability in sulfur content and compliance with 160.333 at each monitoring frequency; nitrogen nonitoring can be valved for pipeline quality natural gas, gines there is no fuel-bound nitrogen and since the free nitrogen does not contribute appreciably to Moy emidsions. Please see the attached sample custom schedulo for datails. Given the increasing trend in the use of pipeline quality natural gas, we are investigating the possibility of asknding subpart OG to allow for loss frequent sulfur monitoring and a valver of nitrogen monitoring requirements where netural gas is need.

Where courses using oil request custom fuel menitoring conseques, Regional Offices are encouraged to contact SECD for consultation on the appropriate fuel menitoring schedule. However, Regions are not required to send the request iteral? to GSCD for appreval.

If you have any questions, please contact sally X. Farrell at YIS 182-2875.

Attachment

od: John Gronehav George Valsh Robert Ajax Tarl Salo

Enclosura

Conditions for Custom Fuel Sampling Schedule for Stationary Gas Turbines

1. Manitoring of fuel nitroyen content shall not be required while naturally is the only fuel fired in the gas turbing.

2. Sulfur Monitoring

- a. Analysis for fuel sulfur content of the natural gas shall be conducted using one of the approved ASTM reference methods for the measurement of sulfur in gaseous fuels, or an approved alternative method. The reference methods are: ASTM D1072-80; ASTM D3031-81; ASTM D3246-81; and ASTM D4084-82 as referenced in 40 CFR 60.335(b)(2).
- b. Effactive the date of this custom schedule, sulfur monitoring shall be conducted twice monthly for six months. If this monitoring shows little variability in the fuel sulfur content. I and indicates consistent compliance with 40 GFR 60.333, then sulfur monitoring shall be conducted once per quarter for six quarters.
- c. If after the menitoring required in item 2(b) above, or herein, the sulfur content of the fuel shows little variability end, calculated as sulfur dioxide, represents consistent compliance with the sulfur dioxide emission limits specified under 40 CFR 60.333, sample analysis shall be conducted twice per annum. This monitoring shall be conducted during the first and third quarters of each calendar year.
- d. Should any sulfur analysis as required in items 2(b) or 2(c) abortaites noncompliance with 40 CPR 60.333, the owner or operator shall notify the State Air Control Board) of such access emissions and the custom schedule shall be re-examined by the Environmental Protection Agency. Sulfur monitoring shall be conducted weekly during the interim period when this custom achequie is being re-examined.
- 3. If there is a change in fuel supply, the owner or operator must notify the State of such change for re-examination of this custom schedule. A substantial change in fuel quality shell be considered as a change in fuel supply. Sulfur monitoring shell be conducted weekly during the interim period when this custom schedule is being re-examined.
- 4. Records of tample analysis and fuel supply pertinent to this custom schedule shall be retained for a period of three years, and be evail for inspection by personnel of federal, state, and local air pollution control agencies.

TOTAL



March 25, 1994

Mr. Chris Kirts Air Program Manager **Northeast District** 7825 Bay Meadows Way, Suite B200 Jacksonville, Florida 32256

Dear Mr. Kirts:

Re: Compliance Test Notification for the University of Florida Cogeneration Project DEP Permit No. AC 01-204652

As required by 40 CFR 60.8, Florida Power Corporation (FPC) is providing the Department of Environmental Protection (DEP) notification of the commencement of compliance testing of the new cogeneration facility at FPC's University of Florida electric generating station. The testing is scheduled to begin on April 25, 1994. If you recall, in a letter dated December 31, 1993, FPC had previously provided notification that testing was to have begun by January 31, 1994. The combustion turbine was damaged during initial startup and debugging and was shipped back to the factory for repair. The April 25, 1994 proposed test date assumes that the refurbished turbine will be received onsite for installation by April 4, 1994.

If you should have any questions concerning this notification, please feel free to contact me at (813) 866-5158.

Sincerely.

Scott H. Osbourn

Senior Environmental Engineer

John Brown, DEP Tallahassee Mike Harley, DEP Tallahassee Mort Benjamin, DEP- Northeast District Patricia Reynolds, Gainesville Air Programs

g. Tranger, EPA

RECEIVED

MAR 3 0 1994

Bureau of Air. Regulation





Florida

Certified Mail P 627 945 297

December 31, 1993

Mr. Chris Kirts Air Program Manager, Northeast District 7825 Bay Meadows Way, Suite B200 Jacksonville, Florida 32256

Dear Mr. Kirts:

Compliance Test Notification for the University of Florida Cogeneration Project Re: DEP Permit No. AC 01-204652

As required by 40 CFR 60.8, Florida Power Corporation (FPC) is providing the Department of Environmental Protection (DEP) notification of the commencement of compliance testing of the new cogeneration facility at FPC's University of Florida electric generating station. The testing is scheduled to begin on January 31, 1994.

A copy of the proposed test plan was received by your office on December 29, 1993. FPC is also submitting a copy of the proposed test plan to Mr. Mike Harley, of the DEP in Tallahassee, with his copy of this letter. Based upon discussions with Messrs. Mort Benjamin and Stan Mazur of your staff on December 30, 1993, FPC will attempt to schedule a pre-test meeting at your office within the next two weeks.

if you should have any questions or concerns, please feel free to contact me at (813) 866-5158.

Sincerely,

Scott H. Osbourn

Senior Environmental Engineer

RECEIVED

JAN 0 3 1954

Bureau of Air Regulation

cc:

John Brown, DEP Tallahassee

Mike Harley, DEP Tallahassee w/Enclosure

GENERAL OFFICE: 3201 Thirty-fourth Street South • P.O. Box 14042 • St. Petersburg, Florida 33733 • (813) 866-5151



Florida Power

Certified Mail P 627 945 298

December 31, 1993

Mr. Chris Kirts Air Program Manager, Northeast District 7825 Bay Meadows Way, Suite B200 Jacksonville, Florida 32256

Dear Mr. Kirts:

Re: Compliance Test Notification for the University of Florida Cogeneration Project DEP Permit No. AC 01-204652

As required by 40 CFR 60, Florida Power Corporation (FPC) is providing the Department of Environmental Protection (DEP) notification of the initial startup of the new cogeneration facility at FPC's University of Florida electric generating station. The initial startup occurred on December 17, 1993.

If you should have any questions or concerns, please feel free to contact me at (813) 866-5158.

Sincerely,

Scott H. Osbourn

Senior Environmental Engineer

cc: John Brown, DEP Tallahassee



Florida

Certified Mail P 627 945 297

December 31, 1993

Mr. Chris Kirts Air Program Manager, Northeast District 7825 Bay Meadows Way, Suite B200 Jacksonville, Florida 32256

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Sincerely,

Scott H. Osbourn

Senior Environmental Engineer

cc: John Brown, DEP Tallahassee

Mike Harley, DEP Tallahassee w/Enclosure

Per David McNeal EPA Region I

RECEIVED

JAN 2 8 1994

 CODE	REFERENCE	QUESTION	AFFECTED REGULATION	DETER- MINATION	Bureau of niscissimRegulation
Λ-41	Meno to R-IV (E. Reich to T. Gibbs) 23 August 77	Is the basis of the existing facility or the basis of the entire stationary source used in the calculation of the annual asset guideline repair allowance, which is referred to in the definition of capital expenditure in Section 60.2(1b)?	60.2 (Eb)		To determine whether or not a modification has occurred due to an increase in production rate, compare the amount of money spent for physical or operational change to the existing facility to the product of the existing facility's basis and the annual asset guideline repair allowance for the existing facility. If more than one existing facility is located in the same stationary source and there is an increase in emissions from both facilities, use the lasts and repair allowance of each separate existing facility for determining whether or not a modification has occurred.
A-42	Meno to R-IV (E. Reich to J. Wa) 29 Sept. 77	What procedure should be followed when an affected facility has not been performance tested in the 180 day period following startup due to shutdowns caused by equipment malfunction?		:	Consider issuing a 113(a) order requiring the owner or operator to notify the Mainistrator upon restartup (by telephone; to be followed by confination in writing) and also requiring a performance test as soon as practicable thereafter but no later than 30 days after restartup. If the facility is mable to operate at the maximum production rate for the initial performance test, a subsequent performance test may be required when the facility achieves maximum production in order to ansure compliance with the standard.
A-43	Memo to R-1V (E. Reich to F. Phillips) 30 Sept. 77	Same as A-39	,		See Λ-39
A-44	Meno to R-VII (E. Reich to E. Stephenson) 28 December 77	Is a steam generator whose capital cost of reconstruction is only 43% of the cost of a comparable new steam generator subject to NSPS due to reconstruction?		No	If the fixed capital cost (including all labor costs) of reconstructing the affected facility (as defined in the applicable subpart) is less than 50% of the cost of an entirely new affected facility, then the affected facility is not subject to NSPS.

FLORIDA POWER CORPORATION UNIVERSITY OF FLORIDA COGENERATION SITE FAX COVER SHEET

P. O. BOX 140660
GAINESVILLE, PL. 32614-0660

PHONE NO. (813) 384-7575 FAX No. (813) 384-7576

TO: Mike Harley

DATE:

1-10-94

FROM: Bob Anderson Number of Pages _____ (Including Cover Sheet)

COMMENTS:

BOB ANDERSON

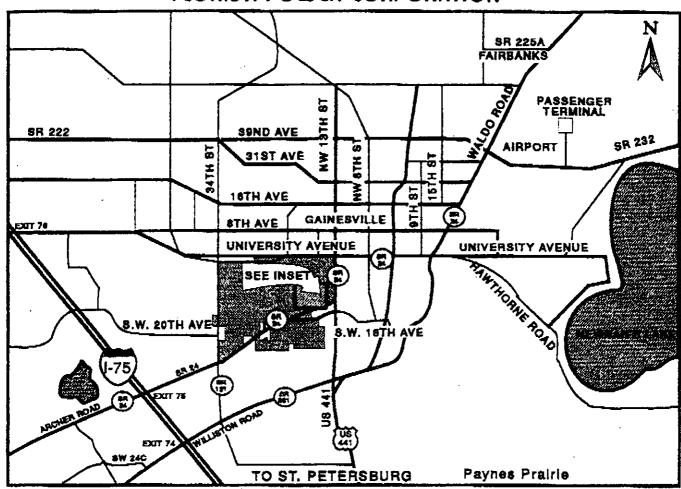
SCOTT OSBORNE

(904)374-2208

TESTINGMA



FLORIDA POWER CORPORATION



Location: Mail Address:

Mowry Road, Gainesville, FI P.O. Box 140660 Gainesville, FL 32614-0660

Nearest Airport:

Gainesville, FL

Driving from GOC:

North on I-75 to Gainesville. Take exit 75 (Archer Rd). Go east 7 traffic lights. Take left on North-South Drive. Go one block to Mowry Rd. Turn right and plant will be on left approx. one block.

Driving from airport: Go west on Rt. 232 (NE 39th Ave.) Turn left on Rt. 441and follow until it merges with Rt. 24. Stay on Rt. 24 past Shands Hospital. Turn right on North-South Drive. Take first right onto Mowry Road and plant will be on left approx. one block.

Telephone:

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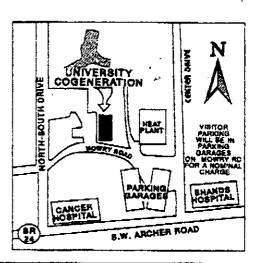
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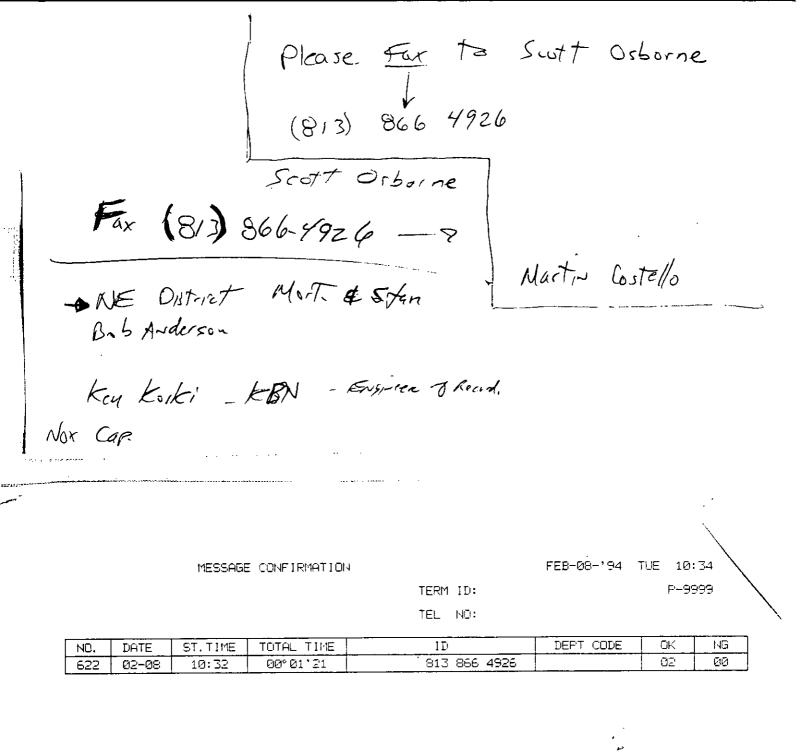
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TEST PLAN

for -

EXHAUST EMISSION MEASUREMENTS

from one

GENERAL ELECTRIC COMBUSTION GAS TURBINE WITH SUPPLEMENTAL FIRED DUCT BURNERS

at the

UNIVERSITY OF FLORIDA FACILITY GAINESVILLE, FLORIDA

> Prepared For Florida Power Corporation December 1993

> > Prepared by



9225 Lockhart Hwy., Austin, Texas 78747 (512) 243-0202 FAX (512) 243-0222

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OVERVIEW

Exhaust emissions from one General Electric (GE) combustion turbine (CT) with supplementally fired heat recovery steam generator (HRSG) are to be tested to determine the quantity of emissions being vented to the atmosphere. The turbine to be tested is in service at the University of Florida facility in Gainesville, Florida, Alachua County. The purpose of this testing is to verify that the turbine demonstrates compliance with the applicable limits set forth by the Florida Department of Environmental Protection (FDEP), air quality permit number AC 01-204652 and PSD-FL-181. The testing will be conducted by Cubix Corporation of Austin, Texas. Table 1 provides background data pertinent to these tests.

The cogeneration unit consists of a GE Model LM 6000 combustion gas turbine (including an inlet air cooler) and a heat recovery steam boiler with supplementary firing duct burners. The turbine and duct burners are fired on pipeline grade natural gas only. The turbine is rated at 43.3 MW when firing natural gas.

NOx emissions from the turbine are controlled by steam injection. Testing will be conducted on the turbine at each of four separate load conditions to verify the steam injection rates at each load. In order to allow the determination of emissions by the duct burner only, two test conditions are required. The first condition tested would be with the combustion turbine (CT) operating at a stabilized full load with the duct burners off. The second condition tested would required the CT (at the same full load rate) and the duct burner to be fired. The NOx emissions from the duct burners would be calculated by subtracting the average NOx emission from the CT only test from the average NOx emission from the CT and duct burner joint fired test.

TABLE 1 Background Data

Sources One GE Model LM 6000 gas combustion

turbine with a supplementary firing HRSG.

This turbine also has inlet air cooling

capabilities.

Location: University of Florida

Mowry Road, Building No. 82

Gainesville, Florida

Applicable Permits FDEP Permit # AC 01-204652

and Regulations PSD-FL-181,

EPA 40 CFR 60 Subparts Db and GG

Emissions Test

<u>Coordinator:</u> Florida Power Corporation

3201 34th Street South

St. Petersburg, Florida 33711 Attn: Albert Morneault, P.E.

(813) 866-5162

<u>Test Contractor:</u> Cubix Corporation

9225 Lockhart Highway Austin, Texas 78747 Attn: Rick J. Krenzke (512) 243-0202 TEL

(512) 243-0222 FAX

<u>Test Dates:</u> To be specified in transmittal letter.

<u>Test Schedule:</u> To be specified in transmittal letter.

TEST MEASUREMENTS

Exhaust emission testing will be conducted on one GE Model LM 6000 gas combustion turbine with a supplementally fired heat recovery steam Emission measurements will be made for NOx, CO, O2, CO2, and opacity on the turbine. Testing will also be performed on the joint firing of the turbine and duct burner to determine the contribution of NOx and CO from the duct burner. All measurements will be conducted while firing natural gas. Compliance tests will be run at 96% to 100% of the maximum capacity achievable for the average inlet air temperature observed during the compliance tests. The turbine manufactures capacity (MW) vs. inlet air temperature curves will be included in the compliance test report. Daily samples of the natural gas will be collected and analyzed for composition, total in sulfur, heating value, and specific gravity. The emission testing will follow the applicable test methods described in the Environmental Protection Agency's (EPA) Code of Federal Regulations, Title 40, Part 60 Appendix A and the fuel analyses will follow analytical procedures set forth by American Society of Testing and Materials (ASTM). The specific test methods to be used are listed as follows:

Exhaust Analyses

- * EPA Method 1 for traverse point layout for the O₂ traverse points established by EPA Method 20.
- * EPA Method 3a for O2 and CO2 concentrations.
- * EPA Method 3b for F_o calculations.
- * EPA Method 9 for opacity observations.
- * EPA Method 10 for CO concentrations.
- * EPA Method 19 for mass emission, and stack flow rate calculations.
- * EPA Method 20 for NOx and O2 concentrations.

Fuel Analyses

- * ASTM D 1945 for natural gas composition analysis.
- * ASTM D 3588 for natural gas specific gravity and heating value (gross and net).
- * ASTM D 3246 for total sulfur content of natural gas.

More detailed descriptions of each test method with any required test method adaptations, as they will be applied to the University of Florida emission tests, are outlined below.

Test Matrix

The test matrix to be used during these tests is depicted in detail in Table 2. Table 2 shows that testing will begin with measurement of the turbine only emissions. The first item during the turbine only tests will be the initial O2 traverse during which O2 and CO2 are measured. Although the actual time of this test run will depend on the stack size, sample port configuration, and the results of Cubix's sample system response time test, it is anticipated that this procedure will require 88-minutes of sampling. This is based on the stack size requiring a 44 point traverse and Cubix's sample system response time being 1-minute or less. EPA Method 20 requires that the sample time at each traverse point be 1-minute plus the average sample system response time. This will result in a 44 point traverse for 2-minutes per point. The sample location for these tests will be from the exhaust stack of the CT/HRSG and the duct burners will be turned off. The O2 traverse will be performed at the lowest load tested with steam injection. Appendix F contains a site-plan, stack drawing, and traverse point layout for this unit.

Following the initial O2 traverse, turbine only emissions will be measured at four separate loads including minimum and maximum firing rates. The four load points will be determined in accordance with 40 CFR 60, Subpart GG, §60.335 (c) (2). These tests are required to satisfy the provisions of EPA Subpart GG and will be conducted from the CT/HRSG stack. Three test runs will be conducted at each of the four loads. Again, Cubix's sample system response time results will determine the actual test run times, but it is anticipated that each test run will consist of 24-minutes (i.e. eight traverse points for 3-minutes per point). NOx, O2, CO2, and CO emissions shall be measured instrumentally and SO2 emissions shall be calculated using the results of the daily fuel analysis. Opacity tests will be conducted during both the CT and the joint fired tests for the time stipulated in 40 CFR 60.11.

Following the turbine only tests at full load, the duct burners shall be turned on to maximum firing rate and the joint fire emissions shall be measured. To satisfy the stipulations of EPA Subpart Db, it is necessary to determine the duct burner contribution to the NOx emissions. The FDEP permit also requires the measurement of the CO emission contribution by the duct burners. With the duct burners firing at maximum, and the turbine operating at the same full load (same MW) as tested prior to the joint firing tests, emissions of NOx and CO will again be measured in the CT/HRSG stack of the unit. In the event that the steam flow cannot be maintained, the CT and duct burner operation may have to be adjusted.

Mass emission rates of the turbine and the duct burners will be calculated by EPA Method 19 procedures. The emission rate from the turbine only are

based on the fuel flow to the turbine, the fuel analysis and exhaust measurements made in the exhaust stack with the turbine only firing. Likewise, the emission rate of the joint firing of the turbine and duct burner are based on the fuel flow to both units, fuel analysis and exhaust measurements make in the CT/HRSG stack. The contribution of the duct burners will be determined by subtracting the turbine only emissions from the joint fired emissions. The contribution from the duct burners will be expressed in lbs/hr and lb/MMBtu for comparison with the permit limits and the NSPS allowable.

Exhaust Gas Sampling and Analyses

The stack gas analyses for NOx, CO, CO₂ and O₂ will be performed by continuous instrumental monitors. Table 3 lists the instruments, detection principles, and applicable ranges of those instruments. All instruments will be housed in an environmentally controlled, trailer-mounted, mobile laboratory. Data from these analyzers will be recorded on two 25-cm width, 3-pen strip chart recorders (Soltec 1243) operating at a speed of 30-cm/hr. A computer data logging system will also be provided to allow for convenient visual checking of emission concentrations. Calibration gases for these instruments will be provided in aluminum cylinders with the concentrations certified by the vendor (See *Quality Assurance Activities*).

The sampling and analysis system to be used for measurement of the above mentioned gaseous concentrations is depicted in Figure 1. Stack gas enters the system through a stainless steel probe with a glass wool filter. The sample is transported via 3/8-inch heat-traced Teflon® tubing to a specially designed stainless steel minimum-contact condenser which dries the sample without removing NOx. The sample is then passed to ground level through 3/8-inch Teflon® via a stainless steel/Teflon® diaphragm pump and into the sample manifold. From the manifold, the sample is partitioned to the analyzers through glass and stainless steel rotometers. The purpose of the rotometers is to ensure that the sample pressure and flow rate are equal to that used for the calibration gases.

Cubix will use a special alloy probe (Haynes Alloy 214) for the sampling of gaseous components. This material has a high yield strength at the elevated temperatures that could be present at these locations and therefore resists bending and warping in the stack.

The tables of EPA Method 1 will be used to locate the traverse points as required for the Method 20 O2 traverse. It is expected that the size and configuration of the combined cycle exhaust stack will require that 44 traverse points be used for the initial O2 traverse. Appendix F of this test plan has

been reserved for stack diagrams and sample traverse point layout schemes.

K-type thermocouples and digital thermometer will be used to measure the stack temperature at each traverse point. This equipment will also be used to measure the stack temperature during all test runs.

The instrumental analysis procedures of EPA Method 3a will be used for determination of O₂ and CO₂ concentrations. The CO₂ analyzer that will be used is based on the principle of infrared absorption; and, the O₂ analyzer operates on a paramagnetic cell. Instrumental analyses will be used in lieu of an Orsat or a Fyrite procedure due to the greater accuracy and precision provided by the instruments.

A calculation technique contained in EPA Method 3b will be used to verify the measured concentrations of O₂ and CO₂. The F₀ calculation of Method 3b will be performed using the measured O₂ and CO₂ concentrations and compared to the expected value published in EPA Method 3b.

EPA Method 10 will be used for measurement of CO concentrations. A continuous nondispersive infrared (NDIR) analyzer will be used for this analysis. This analyzer is equipped with a gas correlation filter which removes any interference from H₂O, CO₂, or other combustion products.

NOx and O2 measurements (as required by Subpart GG) will be made using EPA Method 20. The NOx analyzer to be used operates on the principle of chemiluminescence and the O2 analyzer uses a paramagnetic cell as a detection principle. As required, the NOx analyzer is equipped with an NO2 to NO converter to allow for measurement of all forms of NOx as per EPA's definition. NOx mass emission rates will be calculated as if all the NOx were in the form of NO2. This approach corresponds to EPA's convention, however, it tends to overestimate the actual NOx mass emission rates since the majority of NOx is in the form of NO which has less mass per unit volume (i.e. lbs. of emissions per ppmv concentration) than NO2.

As required by Method 20, an initial O2 traverse will be conducted on the unit while at low load. All subsequent tests will be conducted at the eight points of lowest O2 concentration. Sampling at each traverse point will be conducted for a minimum of 1 minute plus the average sample system response time. The sample system response time will be conducted prior to testing (see *Quality Assurance Activities*); and, based on previous tests, it is expected to be approximately 1 minute. Therefore, Cubix expects to sample for at least 2-minutes per point, making each test run a minimum of 16-minutes in duration (Cubix suggests 24 minute test runs).

Opacity Tests

During these compliance tests, visible emission tests will be performed by FPC certified personnel. To comply with 40 CFR 60.11, three one hour opacity readings will be made while firing turbine only. One 1-hour run will be made at full load, one 1-hour run will be made at the lowest load tested and a final run at an intermediate load. Likewise, while performing the joint firing tests, one 1-hour run will be performed at full load turbine and full fired duct burners. Two more 1-hour runs will be conducted at reduced loads of the duct burner as steam load will allow. Opacity observations shall be made using the procedures of EPA Method 9. FDEP certified personnel (via EPA procedures) shall be used for these opacity observations.

Exhaust Flow Measurements

The stoichiometric calculations of EPA Method 19 will be used to calculate a volumetric flow rate out the exhaust stack. This calculation requires knowledge of the F-factors and heating value of the fuel (as obtained from the fuel composition analysis), and the combustion air rate (as obtained from the diluent concentrations in the stack). Since fuel analyses will not be made until after testing, typical or published values will be used to calculate the volumetric flow rates in presentation of preliminary results. The final emission test report will use the calculated values for F-factors and heating values of each fuel (daily). This strategy will apply to all mass emission rate calculations including the duct burner emission calculations.

Unit Operation Documentation

To document the operational status of the unit during the tests as well as to allow Cubix to calculate stack flow rates, Florida Power Corp. will provide data for each test run. The data that will be recorded at 5-minute intervals, and includes:

- 1) Mean turbine exhaust temperature
- -2) Steam injection rate
- -3) Fuel flow
- 4) Steam/fuel ratio
 - 5) Compressor inlet temperatures
 - 6) Specific humidity
 - 7) Inlet guide vane angle
 - 8) Generator output (MW)
- ≥ 9) Compressor discharge pressure
 - 10) Duct burner fuel flow
 - 11) Stack temperature

Fuel Analyses

The natural gas analyses will consist of measurements of total sulfur and composition. The ASTM methods to be used for this fuel analyses are as follows:

ASTM D 3588 for Heating Value ASTM D 3588 for Specific Gravity ASTM D 3246 for Total Sulfur ASTM D 1945 for Composition of Gas

One natural gas sample will be taken daily, and will be collected in Teflon® lined stainless steel sample "bombs". The total sulfur analyses of the fuel will be used in conjunction with the fuel flow data to indirectly calculate the total SOx (i.e. SO₂) mass emission rates.

Miscellaneous Measurements

Additional measurements to be made by Cubix during each test run include atmospheric pressure (via aneroid aircraft barometer), ambient temperature, and relative humidity as obtained from sling psychrometry (i.e. wet and dry ambient temperatures).

Table 2: Test Matrix

Unit #	<u>Load*</u> <u>I</u>	Duct Burne	<u>er</u>	<u>Parameters</u>	Runs	O2 Traverse
LM 6000	Low			x, <i>CO</i> , O2, VE**		44 pt
LM 6000	Low Int.			ĸ, & Ó, O2, VE**		no
LM 6000	Int.	off	NO	ĸ, <i>Q</i> Ó, O2, VE**	3	no
LM 6000	Full	off	NO	x, &O, O2, VE**	3	no
LM 6000	Full***	100%***	NO	x, CO, O2, VE**	3	no

^{*} Loads will be determined by FPC and will range from minimum load (for O₂ traverse) to full load. Full load depends on the inlet air temperature on the day of the compliance test.

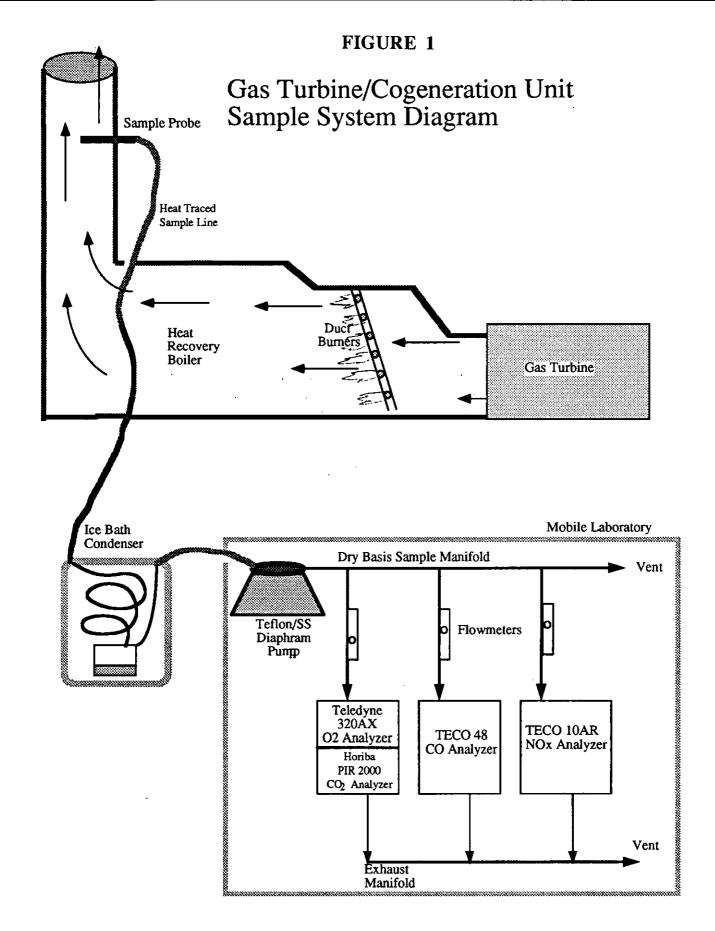
^{**} Three one hour VE runs will be conducted on the turbine only and on the joint firing of the turbine and duct burner (total of 6 one hour runs). One run will be at the lowest load, one run at an intermediate load and one at the highest load. See "Opacity Tests" on page 7 of this workplan.

^{***} This full load condition is dependent on how much steam flow can be dumped. Load for the CT and duct burners may have to be adjusted.

Analytical Instrumentation

<u>Parameter</u>	Model and Manufacturer	Common Use Ranges	Sensitivity	Response <u>Time (sec.)</u>	Detection Principle
NOx	TECO 10AR	0-10 ppm 0-100 ppm 0-200 ppm 0-500 ppm 0-1,000 ppm 0-5,000 ppm	0.1ppm	1.7	Thermal reduction of NO2 to NO. Chemiluminescence of reaction of NO with O3. Detection by PMT. Inherently linear for listed ranges.
CO	TECO 48	0-10 ppm 0-20 ppm 0-50 ppm 0-100 ppm 0-200 ppm 0-500 ppm 0-1000 ppm	0.1ppm	10	Infrared absorption, gas filter correlation detector, microprocessor based linearization
CO ₂	Servomex 1410 B	0-4% 0-20%	0.02%	30	Infrared absorption, analog linearization.
$\overline{\mathrm{O}_2}$	Servomex 1420 B	0-10% 0-25 %	0.1%	15	Paramagnetic cell, inherently linear.

NOTE: Higher ranges available by sample dilution. Other ranges available via signal attenuation.



OUALITY ASSURANCE ACTIVITIES

A number of quality assurance activities will be undertaken prior to, following, and during this testing project. This section of the test plan combined with the example documentation in Appendices C and D describes each of those activities.

Each instrument's response will be checked and adjusted in the field prior to the collection of data via multi-point calibration. The instrument's linearity will be checked by first adjusting its zero and span responses to zero nitrogen and an upscale calibration gas in the range of the expected concentrations. The instrument response will then be challenged with at least one other calibration gas of known concentration. If the instrument's response does not agree with the calibration gases within \pm 2 percent of range, corrective action will be taken prior to beginning the tests.

Each test run will be bracketed by a zero and span check. After each test run, a zero gas and a calibration gas in the range of the span value of the instrument will be introduced to each analyzer to determine the analyzer drift during the run. If the analyzer drifts more than 2% during a test run, that run will be repeated. Appendix C contains an example of a quality assurance worksheet that will be prepared by Cubix to summarize the multi-point linearity check and all zero and span checks.

Interference response tests on the instruments have been conducted by the instrument vendors and/or Cubix Corporation on the NOx, O2, CO2, and CO analyzers. The sum of the interference responses for the stipulated combustion products is less than 2 percent of the applicable full scale span value. The instruments to be used for the tests meet the performance specifications for EPA Methods 3a, 10, and 20. Results of these interference response tests are contained in Appendix C.

The residence time of the sampling and measurement system has been estimated using the pump flow rate and the sampling system volume. The pump's rated flow rate is 0.8 SCFM at 5 psig. The sampling system volume using a typical Cubix sample system has been calculated to be approximately 0.139 scf. Therefore, the minimum sample residence time is less than 11 seconds.

The NOx and O₂ sampling and analysis system will be checked for response time according to the procedures outlined in EPA Method 20. An example data sheet that presents the data from a previous response time check

is included in Appendix C. During this check, the average NOx analyzer's response times were 53.6 seconds upscale and 49.9 seconds downscale. The O₂ analyzer's response times were 55.8 seconds upscale and 32.8 seconds downscale.

Each time the sampling system is set up, a leak check will be conducted prior to testing. The sampling system leak check will demonstrate that a vacuum greater than 10" Hg (probably >20 in Hg) can be held for at least 1 minute with a decline of less than 1" Hg. A leak test will also be conducted before a sample system is dismantled (i.e. after a test series) to ensure that no sample dilution occurred due to ambient air leakage during the tests.

The absence of leaks in the sampling system will also be verified by a sample system bias check. The sampling system's integrity will be tested by comparing the responses of each analyzer to calibration gases introduced via two paths. The first path will be delivered into the analyzer via the zero/span calibration manifold. The second path will consist of introducing a calibration gas into the sample system at the sample probe. Any difference in the instrument responses by these two methods is attributed to sampling system bias or leakage. The sample system bias checks will be conducted as frequently as the leak checks (i.e. after setting up a sample system and prior to dismantling a sample system). The sample system bias checks will demonstrate that no degradation of the sample occurs in the sample system due to absorption, leakage, or contamination.

The efficiency of the NO2 to NO converter in the NOx analyzer will be checked by having the analyzer sample a mixture of NO in N2 standard gas and zero air from a Tedlar® bag. When this bag is mixed and exposed to sunlight, the NO is oxidized to NO2 over a 30 minute period. If the NOx instrument's converter is 100% efficient, then the NOx response will not decrease as the NO in the bag is converted to NO2. The criterion for acceptability is a demonstrated NOx converter efficiency greater than 95%. Strip chart excerpts from previous NOx converter efficiency checks, as well as sample system bias checks, are provided in Appendix G. An example of an Instrumental Quality Assurance Worksheet which summarizes the results of these activities is also included in Appendix C.

The control gases used to calibrate the instruments will be analyzed and certified by the compressed gas vendors to $\pm 1\%$ accuracy. EPA Protocol No. 1 will be used for the NOx gases to assign the concentration values traceable to the National Institute of Standards and Technology (NIST), Standard Reference Materials (SRM's). Examples of calibration gas certifications for a typical turbine test are included in Appendix D.

TEST REPORT AND CALCULATIONS

Test Report

A formal test report documenting the results of the testing program will be prepared after the field testing. The contents of the report will include the following sections:

Introduction: This section will include background data for the tests (i.e. names, addresses, dates, units tested, parameters measured, etc...)

Summary of Results: This section will include tabular summaries of the mass emission rates for NOx (ppmvd, ppmvd at 15% O2, lbs/MMBtu, and lbs/hr), CO (ppmvd, lbs/MMBtu, and lbs/hr), SO2 (lbs/hr) and recorded visible emission results. During the joint fire tests, the duct burner contribution of NOx and CO emissions will be reported in terms of lbs/MMBtu. The permit limits will also be reported for each applicable parameter.

Each tabular summary will also include sections for operational data, fuel data, and ambient conditions. The stack volumetric flow rate as determined from both O2 and CO2 based F-factors will also be included. The mass emission rates will be calculated from the stack flow rate determined by the O2 F-factor. The times and dates of each test run will be noted at the head of each column in the tabular summary. The joint fire tests will be reported separately from the turbine only tests. Appendix A of this test plan is reserved for examples of the tabular summaries for both the turbine and joint-fired tests.

Preceding the tabular summaries, Summary of Results will include text that provides any necessary commentary or explanation of the test results.

Process Description: A brief description of the units tested is provided in this section of the report. Included will be rated operating conditions and stack configuration descriptions. Any applicable model and serial numbers of the unit will also be included.

Analytical Techniques: This section of the report describes the test methods and procedures that were used. This section will closely resemble the Test Measurements section of this test plan.

Quality Assurance Activities: Closely matching the section of this test plan of the same title, this portion of the test report will describe the many QA activities conducted during the tests. The text of this section will be supported by the documents included in the Quality Assurance and Calibration Certifications sections of the Appendix.

Appendices: The supporting documentation will be divided into the following sections:

Appendix A: Field Data Sheets: Stack diagrams, sign-in sheets, templates, preliminary water injection tests, etc...

Appendix B: Example Calculations: Examples of all formulas used for presentation of results in Summary of Results.

Appendix C: Fuel Data: Results of all fuel analyses and Cubix's F-factor and heating value calculation templates.

Appendix D: Operational Data: Computer print-outs supplied by the operator which document the operational status of each unit during each test run. Cubix will mark the test run designations and times of each test run on these print-outs and provide the average operational parameters for each run.

Appendix E: Quality Assurance Activities: Documentation of the various QA Activities conducted for the tests including system response time tests, NOx converter efficiency check strip chart and data sheet, sample system bias checks strip charts and data sheets, interference response checks, etc...

Appendix F: Calibration Certifications: Calibration data for calibration gases, thermometers, altimeter, etc...

Appendix G. Strip Chart Records: Copies of all strip chart recordings made during the tests (if desired).

Appendix H. Opacity Observations: Copies of all opacity field data sheets

Calculations

Emission calculations will be performed by customized spread sheet programs installed on a Macintosh computer. Appendix A of this test plan provides examples of the computer spread sheets Cubix will build for this project. Appendix B shows example calculations of mass emission rates from a turbine only test run and a joint fired test run.

APPENDIX A: EXAMPLE TABLES AND SPREADSHEETS

Example of Natural Gas Fired Test Template

XXXXXXX		ĭ	·-									
XXXXX	~	-										
Solar Taurus Turbine W HRSG											-	
Date												
Turbine #	TCP-2	TCP-2	TCP-2	TCP-2	TCP-2	TCP-2	TCP-2	TCP-2	TCP-2	TCP-2	TCP-2	TCP-2
Test Number	C-16	C-17	C-18	C-19	C-20	C-21	C-22	C-23	C-24	C-25	C-26	C-27
Start Time	847	935	1015	1117	1201	1244	1329	1413	1455	1538	1620	1706
Stop Time	923	1007	1048	1149	1233	1316	1401	1445	1527	1610	1652	1738
Turbine Operational Data												
Power (KW)	2690	2675	2672	3407	3411	3413	3090	3098	3102	2900	2924	2920
Power Turbine Speed (%x 14951=rpm)	100	100	100	100	100	100	100	100	100	100	100	100
T-5 Combustor Temp. (°F)	1207	1203	1202	1400	1400	1400	1400	1330	1329	1283	1284	1281
T-1 Air Inlet Temp. (°F)	62.7	62.7	63.0	69.1	69.5	69.3	69.4	69.7	70.1	70.1	69.0	67.8
Compressor Discharge (psig)	116.0	116.5	116.0	122.0	122.0	122.0	118.0	118.0	118.0	116.0	116.0	116.0
Fuel Flow (SCFM)	712	708	705	844	846	843	790	788	794	753	757	751.3
Fuel Flow (SCFH)	42720	42480	42300	50640	50760	50580	47400	47280	47640	45180	45420	45078
Heat Input (MMBtu/hr)	4.40E+07	4.38E+07	4.36E+07	5.22E+07	5.23E+07	5.21E+07	4.89E+07	4.87E+07	4.91E+07	4.66E+07	4.68E+07	4.65E+07
H2O Flow (gal/min)	1.800	1.800	1.800	2.720	2.700	2.630	2.600	2.230	2.260	2.020	2.040	2.020
H2O-to-fuel Ratio (lb/lb)	0.457	0.457	0.460	0.567	0.570	0.569	0.523	0.521	0.522	0.495	0.495	0.490
Fuel Specific Gravity	0.591	0.591	0.591	0.591	0.591	0.591	0.591	0.591	0.591	0.591	0.591	0.591
Fuel Heating Value (Btu/SCF)	1031	1031	1031	1031	1031	1031	1031	1031	1031	1031	1031	1031
Turbine Sensor Relative Hum. (%)	56.1	56.3	55.8	54.9	52.07	49.4	48.8	48.3	47.6	46.5	45.8	45.9
Turbine Sensor Pbar (in. Hg)	26.4	26.4	26.4	26.5	26.5	26.5	26.4	26.4	26.4	26.4	26.4	26.4
Steam Flow (KPH)	15.63	16.41	16.28	21.11	22.09	20.28	17.79	17.75	17.53	16.8	16.8	16.83
Ambient Conditions												
Barometer (in. Hg)	26.22	26.22	26.22	26.25	26.25	26.25	26.25	26.25	26.15	26.15	26.15	26.15
Temperature (°F dry)	85	85	87	94	96	99	101 ·	102	103	101	107	104
Temperature (°F wet)	60	60	61	67	66	67	68	76	69	68	69	68
Humidity (lbs/lb of air)	0.0066	0.0066	0.0068	0.0096	0.0083	0.0084	0.0087	0.0154	0.0091	0.0088	0.0082	0.0081
Measured Emissions												
NOx (ppmv)	23.4	24.0	24.0	26.0	25.0	26.0	26.0	26.0	25.0	25.0	25.0	23.6
NOx (ppm @ 15% O2)	32.3	33.3	33.2	28.4	27.3	28.4	30.7	31.0	29.8	31.7	31.7	29.9
CO (ppmv)	36.5	39.0	38.0	7.0	7.0	6.5	11.0	12.0	12.0	17.0	17.0	20.0
CO (ppmv @15% O2)	50.4	54.1	52.5	7.6	7.6	7.1	13.0	14.3	14.3	21.6	21.6	25.4
02 (%)	16.63	16.65	16.63	15.50	15.50	15.50	15.90	15.95	15.95	16.25	16.25	16.25
CO2 (%)	2.40	2.40	2.50	3.10	3.10	3.10	2.84	2.80	2.80	2.76	2.80	2.76
Stack Flow Rutes (SCFH)												
O2 Stoichiometry	1.87E+06	1.86E+06		1.75E+06	1.75E+06	1.75E+06	1.77E+06	1.78E+06	1.79E+06	1.81E+06	1.82E+06	1.81E+06
Fuel Fo Factor	1.78	1.77	1.71	1.74	1.74	1.74	1.76	1.77	1.77	1.68	1.66	1.68
Mass Emissions - "F" factor												
NOx (lbs/hr)	5.21 4.94	5.34 5.28	5.29	5.43 0.89	5.23 0.89	5.42 0.82	5.49	5.53 1.55	5.36 1.56	5.41	5.44	5.09
CO (lbs/hr)			5.10				1.41			2.24	2.25	2.62

Example Turbine Template

	Α	В	С	D
1	XXXXXXXX			
2	XXXXXX Cogen Facility			
3	GE Frame 7			
4				
5	Date			
6	Test Series	GTO-3	GTO-3	GTO-3
7	Fuel Type	NG	NG	NG
8	Test Number	C-9	C-10	C-11
9	Start Time	1020	1240	1329
10	Stop Time	1221	1315	1401
11	Turbine Operation			
12	Power (MW)	79.5	78.50	78.5
13	Power Turbine Speed (rpm)	3600	3600	3600
14	Exhaust Temp. (TTXC-°F)	993	994	994
15	Compressor Discharge (psig)	159	159	159
16	Inlet Guide Vanes (degrees)	82	82	82
17	Fuel Flow (lbs/sec)	10.476	10.375	10.422
18	Steam Flow (lbs/sec)	9.677	9.670	9.654
19	Fuel Specific Gravity	0.604	0.604	0.604
20	Fuel Heating Value (Btu/SCF or Btu/lb)	1033	1033	1033
21		830095	822092	825816
22	Ambient Conditions			
23	Barometer (in. Hg)	27.91	27.91	27.91
	Temperature (°F dry)	49	60	63
	Temperature (°F wet)	43	59	59
26	Humidity (lbs/lb of air)	0.0048	0.0110	0.0103
27	Measured Emissions			
28		37.5	37	37.0
29	NOx (ppm @ 15% O2)	37.5	37.0	37.4
30	CO (ppmv)	0.7	0.6	0.6
31	O2 (%)	15.00	15.00	15.06
32	CO2 (%)	3.45	3.45	3.45
33	1.5.5.5.			
	O2 Stoichiometry	2.63E+07	2.61E+07	
	Pitot Tube-Stack	2.63E+07	2.64E+07	2.58E+07
	Mass Emissions (O2 Stoich)			
37	NOx (lbs/hr)	117.86	115.17	116.88
38	1 1	1.34	1.14	1.15
	Mass Emissions (Pitot-Stack)			
40	NOx (lbs/hr)	117.95	116.43	114.02
41	CO (lbs/hr)	1.34	1.15	1.12

Example Joint Fire Turbine Template

	A	В	С	- Б
H	XXXXXXX			
2	XXXXXX			
3	Solar Taurus Turbines W HRSG			
4				
	Date	**CTD-2	ተረጥ ነ	TCD 1
12	Turbine # Test Number	TCP-3	TCP-3 C:14	TCP-3
	Start Time	1412	1530	1650
ٷ ا	Stop Time	1510	1620	1740
10	Turbine Operation - From Solar Instruc	nentation		
11	Power (KW)	3472	3475	3465
12	Power Turbine Speed (%x14951=rpm)	100	100	100
13	T-5 Combustor Temp. (°F) T-1 Air Inlet Temp. (°F)	1400 65.2	1400 64.6	1400 63.9
13	Compressor Discharge (psig)	124	124	124
13	H2O Flow (gal/min)	2.74	2.70	2.70
17	H2O-to-fuel Ratio (lb/lb)	0.592	0.586	0.599
118	Turbine Sensor Relative Hum. (%)	74.9	70.2	67.4
19	Turbine Sensor Pbar (in. Hg)	26.4	26.3	26.3
	Ambient Conditions : Collected by Cubi	x 26.10	26.05	26.05
	Barometer (in. Hg) Temperature (°F dry)	98	100	101
	Temperature (°F vet)	79	81	82
	Humidity (lbs/lb of air)	0.0194	0.0211	0.0219
25	Fuel Flow Data			
26	Turbine NG Fuel Flow (SCFM)	839.4	840.0	841.3
	Turbine NG Fuel Flow (SCFH)	50364	50400	50478
	Turbine NG Fuel Flow (MMBtu/Hr)	51.9	52.0	52.0
129	Fuel Heating Value (Btu/SCF) Fuel Specific Gravity	1031 0.591	1031 0.591	1031 0.591
130	Fuel O2 "F" Factor (DSCF/MMBtu)	8652	8652	8652
	Duct Burner Fuel Flow (SCFM)	164.4	166.0	165.3
33	Duct Burner Fuel Flow (SCFH)	9864	9960	9918
34	Duct Burner Firing Rate (MMBtu/Hr)	10.2	10.3	10.2
35	1802 bires Only Measured Dinitations	30.0		30.0
	NOx (ppmv)	28.0	28.0	29.0
37	NOx (ppm @ 15% O2) CO (ppmv)	30.6 4.0	30.6 5.0	31.7 5.0
			5.0	3.0
1 30	ICO (pressu @15% O2)	1 44	2.5	5.5
39	CO (ppmv @15% O2)	15.50	5.5 15.50	5.5 15.50
40	O2 (%)	4.4 15.50 3.10	5.5 15.50 3.06	5.5 15.50 3.04
40 41 42	O2 (%) CO2 (%) continued on next page	15.50 3.10	15.50 3.06	15.50 3.04
40 41 42 43	O2 (%) CO2 (%) continued on next page Test Number	15.50	15.50	15.50
40 41 42 43 44	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Now Rates (SCFH)	15.50 3.10 C-13	15.50 3.06 C-14	15.50 3.04 C-15
40 41 42 43 44 45	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry	15.50 3.10 C-13	15.50 3.06 C-14	15.50 3.04 C-15
40 41 42 43 44 45 46	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Now Rates (SCFH) O2 Stoichiometry Fuel Fo Factor	15.50 3.10 C-13 1.74E+06 1.74	15.50 3.06 C-14	15.50 3.04 C-15
40 41 42 43 44 45 46 47 48	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Flow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions ** F** fact NOx (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74	15.50 3.06 C-14	15.50 3.04 C-15
40 41 42 43 44 45 46 47 48 49	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Flow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions Fract NOx (lbs/hr) NOx (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12
40 41 42 43 44 45 46 47 48 49 50	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) CO (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11 0.50	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63
40 41 42 43 44 45 46 47 48 49 50 51	O2 (%) CO2 (%) Continued on next page Test Number Turbine Only Flow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) CO (lbs/hr) CO (lbs/MMBtu)	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12
40 41 42 43 44 45 46 47 48 49 50 51 52	O2 (%) CO2 (%) CO2 (%) continued on next page Test Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lbs/hr) CO (lbs/MMBtu) Joint Fired Measured Emissions	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11 0.50 0.01	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01	15.50 3.04 C-15 T.74E+06 1.78 6.03 0.12 0.63 0.01
40 41 42 43 44 45 46 47 48 49 50 51 52 53	O2 (%) CO2 (%) CO2 (%) continued on next page Test Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions - "F" fact NOx (lbs/hr) NOx (lb/MMBtu) CO (lbs/MMBtu) Joint Fired Messured Emissions NOx (ppmv)	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11 0.50	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63
40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/MMBm) Joint Fired Measured Emissions NOx (ppmv) NOx (ppmv) CO (ppmv)	15.50 3.10 C-13 T.74E+06 1.74 or 5.81 0.11 0.50 0.01	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01	15.50 3.04 C-15 T.74E+06 1.78 6.03 0.12 0.63 0.01
40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55	O2 (%) CO2 (%) CO2 (%) continued on next page Test Number Turbine Only Row Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions - "F" fact NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/MMBtu) Joint Fired Measured Emissions NOx (ppmv) NOx (ppmv) NOx (ppmv) @ 15% O2)	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11 0.50 0.01 32.0 28.2	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2
40 41 42 43 44 45 46 47 48 50 51 52 53 54 55 56 57	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions *F* fact NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/MMBtu) Joint Fired Measured Emissions NOx (ppmv) NOx (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv)	15.50 3.10 C-13 T.74E+06 1.74 or 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25
40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 55 56 57 58	O2 (%) CO2 (%) CO2 (%) continued on next page Test Number Turbine Only Row Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lb/MMBtu) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/MMBtu) Joint Fired Measured Emissions NOx (ppmv) NOx (ppmv) NOx (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv)	15.50 3.10 C-13 1.74E+06 1.74 OF: 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2
40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59	O2 (%) CO2 (%) CO2 (%) continued on next page Test Number Turbine Only Flow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions **F** fact NOx (lbs/hr) NOx (lb/MMBtu) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) NOx (ppmv) NOx (ppmv) NOx (ppmv) NOx (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv)	15.50 3.10 C-13 T.74E+06 1.74 9t 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70	15.50 3.04 C-15 T.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72
40 41 42 43 44 45 46 47 48 50 51 52 53 54 55 56 57 58 59 60	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Flow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) Boint Fired Measured Emissions NOx (ppmv) NOx (ppmv) NOx (ppmv) CO (ppmv)	15.50 3.10 C-13 1.74E+06 1.74 9t 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70	15.50 3.04 C-15 T.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72
40 41 42 43 44 45 46 47 48 49 50 51 52 52 53 55 56 60 61	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/MMBtu) Joint Fired Measured Emissions NOx (ppmv) NOx (ppmv @ 15% O2) CO (ppmv) CO (ppmv @ 15% O2) O2 (%) CO2 (%) Joint Fire Flow Rates (SCFH) O2 Stoichiometry Pitot Tube Flow	15.50 3.10 C-13 1.74E+06 1.74 or: 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70	15.50 3.04 C-15 T.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72
40 41 42 43 44 45 46 47 50 51 52 53 54 55 56 61 62 63	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions. "F" fact NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) Hoint Fired Measured Emissions NOx (ppmv) NOx (ppmv @ 15% O2) CO (ppmv) CO (ppmv @ 15% O2) O2 (%) CO2 (%) Joint Fire Flow Rates (SCFH) O2 Stoichiometry Pitot Tube Flow Joint Fired Mass Emissions. "F" factor NOx (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 or: 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70	15.50 3.04 C-15 T.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72
40 41 42 43 44 45 46 47 48 49 50 51 52 52 53 54 61 61 62 63 64	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lb/MMBtu) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/MBtu) Joint Fired Measured Emissions NOx (ppmv) NOx (ppmv @ 15% O2) CO (ppmv) CO (ppmv @ 15% O2) CO (ppmv) Joint Pire Flow Rates (SCFH) O2 Stoichiometry Pitot Tube Flow Home Mass Emissions "F" factor NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr)	15.50 3.10 C-13 T.74E+06 1.74 or 5.81 0.11 0.50 0.01 32.0 28.2 6.0 3.80 1.68E+06 1.75E+06	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06
40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 60 61 62 63 64 65	O2 (%) CO2 (%) continued on next page Test Number Turbins Only Flow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbins Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) Hoastred Emissions NOx (ppmv) NOx (ppmv) NOx (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv @ 15% O2) CO(%) CO2 (%) CO2 (%) CO2 (%) CO3 First Flow Rates (SCFH) O2 Stoichiometry Fitot Tube Flow Joint First Mass Emissions - "F" factor NOx (lbs/hr) CO (lbs/hr)	15.50 3.10 C-13 T.74E+06 1.74 or 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80 1.68E+06 1.75E+06	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06	15.50 3.04 C-15 T.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06
40 41 42 43 44 45 46 47 48 50 51 51 52 53 54 55 56 61 62 63 64 65 66 66 66 66 66 66 66 66 66 66 66 66	O2 (%) CO2 (%) continued on next page Trest Number Turbins Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbins Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hmBm) Joint Fired Measured Emissions NOx (ppmv) NOx (ppmv @ 15% O2) CO (ppmv @ 15% O2) O2 (%) CO2 (%) Joint Fired Mass Emissions CO2 (%) CO2 (%) CO3 (bs/hr) CO4 (bs/hr) Priod Tube Flow Joint Fired Mass Emissions "F" factor NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) CO5 (lbs/hr) CO6 (lbs/hr)	15.50 3.10 C-13 T.74E+06 1.74 or 5.81 0.11 0.50 0.01 32.0 28.2 6.0 3.80 1.68E+06 1.75E+06	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06
40 41 42 43 44 45 46 47 48 50 51 52 53 54 55 56 61 62 63 64 65 66 67	O2 (%) CO2 (%) continued on next page Trest Number Turbins Only Riow Rates (SCPH) O2 Stoichiometry Fuel Fo Factor Turbins Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hmBtu) Joint Fired Measured Emissions NOx (ppmv) NOx (ppmv) CO (ppmv @ 15% O2) CO (ppmv @ 15% O2) O2 (%) CO2 (%) Joint Fire Flow Rates (SCFH) O2 Stoichiometry Pitot Tube Flow Joint Fired Mass Emissions "F" factor NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80 1.68E+06 1.75E+06 6.40 0.63 0.73 0.07	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06 6.47 0.63 0.08	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06 6.67 0.65 0.88
40 41 42 43 44 45 46 47 50 51 52 53 55 55 56 61 62 63 64 66 66 67 68	O2 (%) CO2 (%) continued on next page Test Number Turbins Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (pmv) CO (ppmv) Fired Mass Emissions NOx (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (bs/hr) Fired Mass Emissions - F" factor NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) Fired Mass Emissions - Pitot NOx (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80 1.68E+06 1.75E+06 6.40 0.63 0.73 0.07	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06 6.47 0.63 0.08	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06
40 41 42 43 44 45 46 47 48 50 51 52 53 54 55 56 67 63 69	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions. "F" fact NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/MMBtu) Joint Fired Measured Emissions NOx (ppmv) NOx (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) Fired Measured Emissions O2 (%) CO2 (%) Joint Fire Flow Rates (SCFH) O2 Stoichiometry Fitot Tube Flow Joint Fired Mass Emissions - "F" factor NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) Fired Mass Emissions - Pitot NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOX (lbs/hr) NOX (lbs/hr) NOX (lbs/hr) NOX (lbs/hr) NOX (lbs/hr) NOX (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80 1.68E+06 1.75E+06 6.40 0.63 0.73 0.07	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06 6.47 0.63 0.08	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06 6.67 0.65 0.08
40 41 42 43 44 45 46 47 50 51 52 53 54 55 56 67 62 63 64 65 66 67 69 70	O2 (%) CO2 (%) CO2 (%) continued on next page Test Number Turbins Only Flow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbins Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (pmw) NOx (ppmv) NOx (ppmv) NOx (ppmv) NOx (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO2 (%) CO2 (%) CO2 (%) CO2 (%) CO3 (bs/hr) CO (lbs/hr) NOx (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80 1.68E+06 1.75E+06 6.40 0.63 0.73 0.07	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06 6.47 0.63 0.08	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06
40 41 42 43 44 45 46 47 50 51 52 53 54 55 56 57 58 61 62 63 63 64 67 71 72	O2 (%) CO2 (%) CO2 (%) continued on next page Test Number Turbine Only Riow Rates (SCPH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hmBtu) Joint Fired Measured Emissions NOx (ppmv) NOx (ppmv) CO (ppmv @ 15% O2) CO (ppmv) CO (ppmv @ 15% O2) O2 (%) Joint Fire Flow Rates (SCFH) O2 Stoichiometry Pitot Tube Flow Joint Pired Mass Emissions "F" factor NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 0E 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80 1.68E+06 1.75E+06 6.40 0.63 0.73 0.07 6.67 0.66 0.76 0.07	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06 6.47 0.08 0.08	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06 6.67 0.86 0.08
40 41 42 43 44 45 46 47 48 50 51 52 53 54 61 62 63 64 65 67 70 71 72 72 73	O2 (%) CO2 (%) continued on next page Trest Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hMBm) Joint Fired Measured Emissions NOx (ppmv) CO (ppmv @ 15% O2) CO (ppmv) CO (ppmv @ 15% O2) O2 (%) CO2 (%) Joint Fire Flow Rates (SCFH) O2 Stoichiometry Pitot Tube Flow Joint Fired Mass Emissions "F" factor NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 OE 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80 1.68E+06 1.75E+06 6.40 0.63 0.73 0.07 6.67 0.66 0.76 0.07	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06 6.47 0.63 0.08 6.97 0.68 0.09	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06 6.67 0.68 0.08
40 41 42 43 44 45 46 47 50 51 52 53 54 61 62 63 64 65 67 70 71 72 72 73 74	O2 (%) CO2 (%) continued on next page Trest Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (ppmv @ 15% O2) CO (ppmv) CO (ppmv @ 15% O2) CO (ppmv @ 15% O2) O2 (%) CO2 (%) GO2 (%) GO2 (%) Joint First How Rates (SCFH) O2 Stoichiometry Pitot Tube Flow Joint First Mass Emissions "F" factor NOx (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80 1.68E+06 1.75E+06 6.40 0.63 0.73 0.07 6.67 0.666 0.76 0.07	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06 6.47 0.63 0.08 0.08	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06 6.67 0.65 0.08 6.98 0.08
40 41 42 43 44 45 46 47 48 50 51 52 53 55 55 56 61 62 63 64 65 69 70 71 72 73 73 74 75	O2 (%) CO2 (%) continued on next page Test Number Turbins Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (pmv) CO (ppmv) First Flow Rates (SCFH) O2 Stoichiometry Pitot Tube Flow Joint First Mass Emissions "F" factor NOx (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80 1.68E+06 1.75E+06 6.40 0.63 0.73 0.07 6.67 0.66 0.76 0.07	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06 6.47 0.63 0.08 0.08 0.08 0.08 0.08 0.09	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06 6.67 0.65 0.86 0.08 0.90 0.09
40 41 42 43 44 45 46 47 48 50 51 55 55 57 58 59 60 61 62 63 64 65 67 71 72 73 74 75 76	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions. "F" fact NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (ppmv) O2 (%) CO2 (%) CO2 (%) CO2 (%) CO1 (ppmv @ 15% O2) O2 (%) CO2 (%) CO2 (%) CO3 (bs/hr) CO (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80 1.68E+06 1.75E+06 6.40 0.63 0.73 0.07 6.67 0.666 0.76 0.07	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06 6.47 0.63 0.08 0.08	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06 6.67 0.65 0.08 6.98 0.08
40 41 42 43 44 45 46 47 50 51 52 53 54 55 55 56 57 58 60 61 62 63 64 65 66 67 70 71 72 73 74 75 76 77 77 76 77	O2 (%) CO2 (%) CO2 (%) continued on next page Test Number Turbine Only Flow Rates (SCPH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions "F" fact NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hmBtu) Joint Fired Measured Emissions NOx (ppmv) NOx (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv) CO (ppmv @ 15% O2) O2 (%) Joint Fire Flow Rates (SCFH) O2 Stoichiometry Pitot Tube Flow Joint Fired Mass Emissions - "F" factor NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 OE 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80 1.68E+06 1.75E+06 6.40 0.63 0.73 0.07 6.67 0.66 0.76 0.07 0.59 0.06 0.23 0.02	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06 6.47 0.08 0.08 0.08 0.09	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06 0.65 0.08 0.08 0.08
40 41 42 43 44 45 46 47 50 51 52 53 54 55 56 57 58 61 62 63 64 67 71 72 73 74 75 77 77 78	O2 (%) CO2 (%) continued on next page Test Number Turbine Only Riow Rates (SCFH) O2 Stoichiometry Fuel Fo Factor Turbine Only Mass Emissions. "F" fact NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (ppmv) O2 (%) CO2 (%) CO2 (%) CO2 (%) CO1 (ppmv @ 15% O2) O2 (%) CO2 (%) CO2 (%) CO3 (bs/hr) CO (lbs/hr)	15.50 3.10 C-13 1.74E+06 1.74 or 5.81 0.11 0.50 0.01 32.0 28.2 6.0 5.3 14.20 3.80 1.68E+06 1.75E+06 6.40 0.63 0.73 0.07 6.67 0.66 0.76 0.07	15.50 3.06 C-14 1.74E+06 1.76 5.82 0.11 0.63 0.01 32.0 28.4 7.0 6.2 14.25 3.70 1.69E+06 1.82E+06 6.47 0.63 0.08 0.08 0.08 0.08 0.08 0.09	15.50 3.04 C-15 1.74E+06 1.78 6.03 0.12 0.63 0.01 33.0 29.3 7.0 6.2 14.25 3.72 1.69E+06 1.77E+06 6.67 0.65 0.86 0.08 0.90 0.09

Example Joint Fired Template

	Ä	В	С	D
1	XXXXXXX			
	GTO3 Joint Firing Tests			
	Date		2.42	
	Test Number	C-12	C-13	C-14
	Start Time	1738	1838	1926
6	Stop Time	1830	1918	1956
7	Unit Operation Power (MW)	76.9	76.5	76.5
8	Average Turbine Exhaust Temperature (°F)	997	996	997
	Steam Injection (lbs/sec.)	8.990	9.047	9.055
	Steam/Fuel Ratio (lb/lb)	0.88	0.88	0.88
	Turbine NG Fuel Flow (lbs/sec)	10.244	10.251	10.233
	Turbine Fuel Flow (MMBtu/hr)	822.50	823.06	821.62
14	Fuel Heating Value (Btu/lb)	22303	22303	22303
15	Fuel O2 F Factor	8666	8666	8666
16	Fuel CO2 F Factor	1032	1032	1032
17	HRSG Duct Burner Fuel Flow (lb/hr)	5928	5928.0	5928.0
18	Fuel Heating Value (Btu/lb)	21746	21746	21746
19	Fuel O2 F Factor	8666	8666	8666
20	Fuel CO2 F Factor	1032	1032	1032
	Duct Burner Firing Rate (MMBtu/hr)	129	129	129
	Ambient Conditions			
	Barometer (in. Hg)	27.91	27.91	27.91
24	Temperature (°F dry)	63	64	61
25	Temperature (°F wet)	60	61	59
	Humidity (lbs/lb of air)	0.0110	0.0114	0.0108
	Turbine Measured Emissions (dry basis)	40.4	40.0	41.1
	NOx (ppmv) NOx (ppmv @ 15% O2)	40.4	40.0	41.1
	CO (ppmv)	0.6	0.6	0.6
	O2 (%)	15.00	15.00	15.00
	CO2 (%)	3.53	3.51	3.52
	Turbine Duct Flow Rates (DSCFH)	2.23	3.31	3.52
	EPA Fo Factor	1.67	1.68	1.68
	O2 Stoichiometry	2.52E+07		2.52E+07
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	ICO2 Stoichiometry	2.40E+07	2.42E+07	2.41E+07
	CO2 Stoichiometry Turbine Mass Emissions (O2 F Fact.)	2.40E+07	2.42E+07	2.41E+07
37	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr)	2.40E+07 121.80	2.42E+07 120.67	2.41E+07 123.77
37 38	Turbine Mass Emissions (O2 F Fact.)			
37 38 39 40	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/MMBtu) CO (lbs/hr)	121.80 0.15 1.10	120.67 0.15 1.10	123.77 0.15 1.10
37 38 39 40 41	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/MMBtu) CO (lbs/hr) CO (lbs/MMBtu)	121.80 0.15	120.67 0.15	123.77 0.15
37 38 39 40 41 42	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/MMBtu) CO (lbs/hr) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.)	121.80 0.15 1.10 0.0013	120.67 0.15 1.10 0.0013	123.77 0.15 1.10 0.0013
37 38 39 40 41 42 43	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/MMBtu) CO (lbs/hr) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr)	121.80 0.15 1.10	120.67 0.15 1.10	123.77 0.15 1.10
37 38 39 40 41 42 43	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/MMBtu) CO (lbs/hr) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis)	121.80 0.15 1.10 0.0013	120.67 0.15 1.10 0.0013	123.77 0.15 1.10 0.0013
37 38 39 40 41 42 43 44	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/MMBtu) CO (lbs/hr) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv)	121.80 0.15 1.10 0.0013 115.99	120.67 0.15 1.10 0.0013 115.58	123.77 0.15 1.10 0.0013 118.21
37 38 39 40 41 42 43 44 45	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/MMBtu) CO (lbs/MMBtu) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6	120.67 0.15 1.10 0.0013 115.58 41.3 2.9	123.77 0.15 1.10 0.0013 118.21 42 3.5
37 38 39 40 41 42 43 44 45 46 47	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/MMBtu) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86
37 38 39 40 41 42 43 44 45 46 47	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hm) CO (lbs/hm) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%) CO2 (%)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6	120.67 0.15 1.10 0.0013 115.58 41.3 2.9	123.77 0.15 1.10 0.0013 118.21 42 3.5
37 38 39 40 41 42 43 44 45 46 47 48 49	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/MMBtu) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21
37 38 39 40 41 42 43 44 45 46 47 48 49 50	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hm) CO (lbs/hm) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hmBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hm/Btu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/MMBtu) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) CO (ppmv) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 2.28E+07	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/MMBtu) CO (lbs/MMBtu) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.) NOx (lbs/hr)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/MMBtu) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) CO (ppmv) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 2.28E+07	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 2.28E+07	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07 122.63 0.13
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/MMBtu) CO (lbs/MMBtu) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) CO (2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07 115.39 0.12 6.09 0.006	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 2.39E+07 118.09 0.12 5.04	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07 122.63 0.13 6.21
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 55 56 57 58	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/MMBtu) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/MMBtu) Joint Fire Mass Emissions (CO2 F Fact.) NOx (lbs/hr)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07 115.39 0.12 6.09	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 2.39E+07 118.09 0.12 5.04	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07 122.63 0.13 6.21
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 55 56 57 58	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/MMBtu) Joint Fire Mass Emissions (CO2 F Fact.)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07 115.39 0.12 6.09 0.006	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 2.28E+07 118.09 0.12 5.04 0.005	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07 122.63 0.13 6.21 0.007
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hm/Btu) CO (lbs/hm/Btu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hm/Btu) CO (lbs/hr) CO (lbs/hr) Duct Burner Contribution (O2 F Fact.) NOx (lbs/hr) Duct Burner Contribution (O2 F Fact.)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07 115.39 0.12 6.09 0.006	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 2.28E+07 118.09 0.12 5.04 0.005	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07 122.63 0.13 6.21 0.007
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/MMBtu) CO (lbs/MMBtu) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/hr) Duct Burner Contribution (O2 F Fact.) NOx (lbs/hr) via O2 F Factor NOX (lbs/hr) via O2 F Factor	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07 115.39 0.12 6.09 0.006	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 2.28E+07 118.09 0.12 5.04 0.005	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07 122.63 0.13 6.21 0.007 116.85
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/MMBtu) CO (lbs/MMBtu) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hmBtu) Joint Fire Mass Emissions (CO2 F Fact.) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) Duct Burner Contribution (O2 F Fact.) NOx (lbs/hr) via O2 F Factor NOx (lbs/hr) via CO2 F Factor NOx (lbs/hr) via CO2 F Factor	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07 115.39 0.12 6.09 0.006 113.67 -6.41 -2.32 -0.050	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 2.28E+07 118.09 0.12 5.04 0.005 112.40 -2.58 -3.17 -0.020	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07 122.63 0.13 6.21 0.007 116.85 -1.14 -1.36 -0.009
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/MMBtu) CO (lbs/MMBtu) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/MMBtu) Joint Fire Mass Emissions (CO2 F Fact.) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) Duct Burner Contribution (O2 F Fact.) NOx (lbs/hr) via O2 F Factor NOx (lbs/hr) via CO2 F Factor NOx (lbs/MMBtu O2 F factor) NOx (lbs/MMBtu O2 F factor)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07 115.39 0.12 6.09 0.006 113.67 -6.41 -2.32 -0.050 -0.018	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 118.09 0.12 5.04 0.005 112.40 -2.58 -3.17 -0.020 -0.025	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07 122.63 0.13 6.21 0.007 116.85 -1.14 -1.36 -0.009 -0.011
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 60 61 62 63 64 65	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/MMBtu) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hmBtu) Joint Fire Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Duct Burner Contribution (O2 F Fact.) NOx (lbs/hr) via O2 F Factor NOx (lbs/hr) via CO2 F Factor NOx (lbs/hr) via CO2 F factor)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07 115.39 0.12 6.09 0.006 113.67 -6.41 -2.32 -0.050 -0.018 4.99	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 2.28E+07 118.09 0.12 5.04 0.005 112.40 -2.58 -3.17 -0.020 -0.025 3.94	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07 122.63 0.13 6.21 0.007 116.85 -1.14 -1.36 -0.009 -0.011 5.12
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64 65 66	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/MMBtu) CO (lbs/MMBtu) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) Duct Burner Contribution (O2 F Fact.) NOx (lbs/hr) via O2 F Factor NOx (lbs/hr) via CO2 F Factor NOx (lbs/hr) via CO2 F factor) NOx (lbs/hr) NOx (lbs/hr) via CO2 F factor) NOx (lbs/hr) NOx (lbs/hr) via CO2 F factor) NOx (lbs/hr) NOx (lbs/MMBtu CO2 F factor) NOx (lbs/hr) CO (lbs/hr)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07 115.39 0.12 6.09 0.006 113.67 -6.41 -2.32 -0.050 -0.018	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 118.09 0.12 5.04 0.005 112.40 -2.58 -3.17 -0.020 -0.025	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07 122.63 0.13 6.21 0.007 116.85 -1.14 -1.36 -0.009 -0.011
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 67 60 61 62 63 64 66 67	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Joint Fire Measured Emissions (dry basis) NOx (ppmv) CO (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) Duct Burner Contribution (O2 F Fact.) NOx (lbs/hr) Duct Burner Contribution (O2 F Fact.) NOx (lbs/hr) via O2 F Factor NOx (lbs/hr) via CO2 F Factor NOx (lbs/hr) NOX (lbs/hr) NOX (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr) CO (lbs/hr)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07 115.39 0.12 6.09 0.006 113.67 -6.41 -2.32 -0.050 -0.018 4.99 0.039	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 2.28E+07 118.09 0.12 5.04 0.005 112.40 -2.58 -3.17 -0.020 -0.025 3.94 0.031	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07 122.63 0.13 6.21 0.007 116.85 -1.14 -1.36 -0.009 -0.011 5.12 0.040
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 67 61 62 63 64 65 66	Turbine Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hr) Turbine Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Nox (lbs/hr) Joint Fire Mass Emissions (dry basis) NOx (ppmv) CO (ppmv) O2 (%) CO2 (%) Joint Fire Stack Flow Rates (DSCFH) EPA Fo Factor O2 Stoichiometry CO2 Stoichiometry CO2 Stoichiometry Joint Fire Mass Emissions (O2 F Fact.) NOx (lbs/hr) NOx (lbs/hr) CO (lbs/hr) CO (lbs/hmBtu) Joint Fire Mass Emissions (CO2 F Fact.) NOx (lbs/hr) Duct Burner Contribution (O2 F Fact.) NOx (lbs/hr) via O2 F Factor NOx (lbs/hr) via CO2 F Factor NOx (lbs/hr) via CO2 F Factor NOx (lbs/hr) NOx (lbs/hr) NOx (lbs/MMBtu O2 F factor) CO (lbs/hr) CO (lbs/MMBtu) Method 19 NOx (lbs/MMBtu)	121.80 0.15 1.10 0.0013 115.99 41.5 3.6 13.50 4.28 1.73 2.33E+07 2.29E+07 115.39 0.12 6.09 0.006 113.67 -6.41 -2.32 -0.050 -0.018 4.99	120.67 0.15 1.10 0.0013 115.58 41.3 2.9 13.7 4.31 1.67 2.39E+07 2.28E+07 118.09 0.12 5.04 0.005 112.40 -2.58 -3.17 -0.020 -0.025 3.94	123.77 0.15 1.10 0.0013 118.21 42 3.5 13.86 4.21 1.67 2.45E+07 2.33E+07 122.63 0.13 6.21 0.007 116.85 -1.14 -1.36 -0.009 -0.011 5.12

O2 F Factor Calculation: Example - Natural Gas

Client: XXXXXXXXXXX

Sample ID: Natural gas fired turbine

Time: XXXXX Date: XXXXXX

				% volume		Component		Gross	Volume
	%	Molecular	Density	x		Gross	Weight	Heating Value	Fract.
Componen	Volume	Wt.	(lb/ft3)	Density	weight %	Btu/lb	Fract. Btu	(Btu/SCF)	Btu
Hydrogen	0.0000	2.016	0.0053	0.00000	0.0000	61100	0.00	325	0
Oxygen	0.0000	32.000	0.0846	0.00000	0.0000	0	0.00	0	
Nitrogen	1.7400	28.016	0.0744	0.00129	2.8623	0	0.00	0	0
CO2	0.4700	44.01	0.117	0.00055	1.2158	0	0.00	0	0
∞	0.0000	28.01	0.074	0.00000	0.0000	4347	0.00	322	0
Methane	93.9100	16.041	0.0424	0.03982	88.0370	23879	21022.35	1013	951.308
Ethane	3.0900	30.067	0.0803	0.00248	5.4861	22320	1224.49	1792	55.3728
Ethylene	0.0000	28.051	0.0746	0.00000	0.0000	21644	0.00	1614	0
Propane	0.5500	44.092	0.1196	0.00066	1.4544	21661	315.04	2590	14.245
propylene	0.0000	42.077	0.111	0.00000	0.0000	21041	0.00	2336	0
Isobutane	0.0600	58.118	0.1582	0.00009	0.2099	21308	44.72	3363	2.0178
n-butane	0.0900	58,118	0.1582	0.00014	0.3148	21257	66.92	4016	3,6144
Isobutene	0.0000	56.102	0.148	0.00000	0.0000	20840	0.00	3068	0
Isopentane	0.0200	72.144	0.1904	0.00004	0.0842	21091	17.76	4008	0.8016
n-pentane	0.0200	72.144	0.1904	0.00004	0.0842	21052	17.72	3993	0.7986
n-hexane	0.0500	86.169	0.2274	0.00011	0.2514	20940	52.64	4762	2.381
H2S		34.076	0.0911	0.00000	0.0000	7100	0.00	647	0
total	100.00	Averag	e Density	0.04523	100.0000	Gross Heatin	g Value_	Gross Heating \	/alue
		Specif	ic Gravity	0.59122		Btu/lb	22762	Btu/SCF	1031

•		FACTORS :	•				Weigh	t Percents	
Componen	Mol. Wt.	C Factor	H Factor	% volume	Fract. Wt.	Carbon	Hydrogen	Nitrogen	Oxygen
Hydrogen	2.016	0	1	0.00	0.0000	0	0		
Oxygen	32	0	0	0.00	0.0000				0
Nitrogen	28.016	0	0	1.74	48.7478	0	0	2.85257	
CO2	44.01	0.272273	0	0.47	20.6847	0.32955963	0		0.87996
∞	28.01	0.42587	0	0.00	0.0000	0	0		0
Methane	16.041	0.75	0.25	93.91	1506.4103	66.1126772	22.037559		
Ethane	30.067	8.0	0.2	3.09	92.9070	4.349294	1.0873235		
Ethylene	28.051	0.85714	0.14286	0.00	0.0000	0	0		
Propane	44.092	0.81818	0.18182	0.55	24.2506	1.16105167	0.2580118		
Propene	42.077	0.85714	0.14286	0.00	0.0000	0	0		
Isobutane	58.118	0.82759	0.17247	0.06	3.4871	0.16887188	0.035193		
n-butane	58.118	0.82759	0.17247	0.09	5.2306	0.25330782	0.0527894		
Isobutene	56.102	0.85714	0.14286	0.00	0.0000	0	0		
isopentane	72.144	0.83333	0.16667	0.02	1.4429	0.07036026	0.0140724		
n-pentane	72.144	0.83333	0.16667	0.02	1.4429	0.07036026	0.0140724		
n-hexane	86.169	0.83721	0.16279	0.05	4.3085	0.21107445	0.041042		
H2S	34.08	0	0	0.00	0.0000	0	0		
Totals				100.00	1708.9124	72.7265572	23.54	2.85257	0.87996
		CALCULAT	ED VALUE	S					
		O2 F Facto	or (dry)	8653	DSCF of Exh	aust/MM Btu o	f Fuel Burned (@ 0% excess aii	r
		O2 F Facto	or (wet)	10649	SCF of Exha	ust/MM Btu of	Fuel Burned @	0% excess air	
		Moisture F		1996	SCF of Wate	r/MM Btu of Fu	iel Burned @ 0	% excess air	
		Combust.	Moisture	18.7			@ 0% excess		
		CO2 F Fac	tor	1026	DSCF of CO	2/MM Btu of Fu	el Burned @ 0	% excess air	

APPENDIX B: EXAMPLE CALCULATIONS

Turbine Exhaust Concentration Standards

(40CFR60 Subpart GG and Appendix A, Method 20)

Date: XXXXX

Plant: XXXXXXXX Corporation
Stack: Solar Taurus Turbine TCP-3

Technician: RK, TS, LI

Calculate NO_x Emission Concentration Standard

For turbines having fuel flows at peak load between 10 and 100 MMBtu/hr:

ppmv NO_x Standard =
$$\left\{ 150 \times \left(\frac{13658 \left(\frac{Btu}{Kw-hr} \right)}{Y} \right) + F \right\}$$

where:

- Y = Measured or manufacturer's rated efficiency in terms of lower heating value of fuel in $\left(\frac{Btu}{Kw-hr}\right)$ at actual peak load. (10,180 Btu/Hp-hr = 14.4 Kilojoules/Watt-hr = 13,658 Btu/Kw-hr). "Y" can not be greater than these values.
- $F = Adjustment to NO_x$ concentration standard (ppm) according to fuel bound nitrogen content (excluding gaseous N_2).

Y (actual value) =
$$13284 \left(\frac{Btu}{Kw-hr} \right)$$
 based on Run C-8 at full load.

ppmv NO_x Standard =
$$\left\{ 150 \times \left(\frac{13658 \left(\frac{Btu}{Kw-hr} \right)}{13284 \left(\frac{Btu}{Kw-hr} \right)} \right) + 0 \right\} = 154.2 \text{ ppmv}$$

NO_x Adjustment to 15% O₂ and NO_x (EPA Corrected)

Date: XXXXX

Plant: XXXXXXXX

Stack: Solar Taurus Turbine TCP-3

Technician: RK, TS, LI

Example Test Run: C-13

Measured Concentrations: NO_x (ppmv) 28.0

O₂ (%) 15.5

Calculation to Adjust NO_X to 15% O₂

 NO_x @ 15% $O_2 = NO_x$ measured (ppmv) $\times \left(\frac{5.9}{20.9 - O_2\% \text{ measured}}\right)$

=28.0 × $\left(\frac{5.9}{20.9 - 15.5\%}\right)$ = 30.6 ppmv @ 15% O₂

O2 Based F Factor Emission Calculations for Natural Gas

Date: XXXXX

Plant: XXXXXXXXX

Stack: Solar Taurus Turbine TCP-3

Technician: RK, TS, SB

Example Test Run: C-13

Measured Concentrations: NO_x (ppmv) 28.0

O₂ (%) 15.5

Fuel Flow = $50364 \left(\frac{SCF}{hr} \right)$

Gross Heating Value = $1031 \left(\frac{Btu}{SCF} \right)$

 F_1 Factor = 8652 $\left(\frac{DSCF}{MMBtu}\right)$

Heat Flow Rate Calculation

$$Z_1\left(\frac{\text{MMBtu}}{\text{hr}}\right)$$
 = Fuel Flow $\left(\frac{\text{SCF}}{\text{hr}}\right) \times$ Gross Heating Value $\left(\frac{\text{Btu}}{\text{SCF}}\right) \times 10^{-6}$
= 50364 $\left(\frac{\text{SCF}}{\text{hr}}\right) \times 1031 \left(\frac{\text{Btu}}{\text{SCF}}\right) \times 10^{-6}$
= 51.96 $\left(\frac{\text{MMBtu}}{\text{hr}}\right)$

Stack Gas Flow Calculation

$$Q_{d}\left(\frac{DSCF}{hr}\right) = \left\{\frac{Z_{1} \times F_{1} \times 20.9}{20.9 - O_{2}\%}\right\} = \left\{\frac{52.98\left(\frac{MMBtu}{hr}\right) \times 8652\left(\frac{DSCF}{MMBtu}\right) \times 20.9}{20.9 - 15.50\%}\right\}$$
$$= 1,738,793\left(\frac{DSCF}{hr}\right)$$

Emissions in (lbs/hr) Calculation via O2 Stoichiometry

$$\left(\frac{\text{lbs}}{\text{hr}}\right) = \left\{ \text{Conc. (ppmv)} \times 10^{-6} \times \text{M.W.} \left(\frac{\text{lbs}}{\text{lb-mole}}\right) \times 385.15^{-1} \left(\frac{\text{lb-mole}}{\text{DSCF}}\right) \times Q_d \left(\frac{\text{DSCF}}{\text{hr}}\right) \right\}$$

NOx
$$\left(\frac{\text{lbs}}{\text{hr}}\right) = \left\{28.0 \text{ ppmv} \times 10^{-6} \times 46 \left(\frac{\text{lbs}}{\text{lb*mole}}\right) \times 385.15^{-1} \left(\frac{\text{lb*mole}}{\text{DSCF}}\right) \times 1.74 \times 10^{6} \left(\frac{\text{DSCF}}{\text{hr}}\right)\right\}$$

$$= 5.81 \left(\frac{\text{lbs}}{\text{hr}}\right)$$

Duct Burner contribution to Emissions

Refers to Test Run C-13

Ebo = Duct Burner contribution (lb/MMBtu)

Qft = fuel flow to turbine = 50,364 SCF/hr

BTUt = heating value of turbine fuel = 1031 BTU/SCF

Hg = heat input to turbine = Qft x BTUt = 51.9 MMBTU/h

Qfb = fuel flow to boiler = 9864 SCF/hr

BTUb = heating value of boiler fuel = 1031 BTU/SCF

Hb = heat input to boiler = Qfb x BTUb = 10.2 MMBTU/hr

Eg = pollutant rate from turbine = 5.81 lbs/hr = 0.11 lbs/MMBTU

Eco = pollutant rate from joint fire =6.4 lbs/hr= .63 lbs/MMBTU

*CO emissions calculated using same formula with appropriate CO emissions.

Calculations for Gaseous Emissions QA

Certified Gas Input

Concentration (% or ppmv) = concentration of gas from vendor certification

Target (% Chart) =
$$\left\{ \frac{\text{Concentration} \times 100}{\text{Full Scale}} \right\} + \text{zero offset} \right\}$$

For 160.9 ppmv NO_x, Target (% Chart) =
$$\left\{ \left(\frac{160.9 \times 100}{200} \right) + 2.0 \right\} = 82.45$$

Initial Calibration and Linearity Check

Initial (% chart) = observed reading when calibration gas is analyzed

Difference (% chart) = Initial (% chart) - Target (% chart)

For 160.9 NO_x, Difference (% chart) = 83.00 - 82.45 = 0.55

Test Run C-1

Average ppmv calculated from strip chart = (observed – zero offset) $\times \left\{ \frac{\text{Full Scale}}{100} \right\}$ =(14.0 - 2) $\times \left\{ \frac{200}{100} \right\}$ = 24.0 ppmv

Calibration Check Run 403.8 ppmv NO_x C-1

*The drift is considered to be acceptable within 2% of chart.

APPENDIX C: EXAMPLE QUALITY ASSURANCE ACTIVITIES

Instrumental Analysis Quality Assurance Data

Plant: Technician: TS

NOx Analyzer: NO2 to NO Converter Efficiency Test

	NOx Concentration (ppm)	% Decrease from Initial Concentration	NO Concentration (ppm)
Initial Concentration	85.0	0.0	66.0
10 minute Concentration	85.6	-0.3	61.0
20 minute Concentration	86.0	-0.2	59.0
30 minute Concentration	86.4	-0.2	56.0
Full Scale: 200			

Sample System Bias Check

Bampic Bysu	cili Dias Cilcen				
	Calibration	Full Scale	Direct	Sample	Sample
	Gas	Span	Calibration	System	System
	Concentration	-	Response	Response	Bias
	(ppm)	(ppm)	(ppm)	(ppm)	(% of Span)
Parameter					
NOx	160.9	200	161.0	162.2	0.65
NOx	160.9	200	161.0	161.4	0.25
NOx	160.9	200	160.2	160.8	-0.05
NOx	160.9	200	161.4	161.0	0.05
NOx	160.9	200	161.0	161.2	0.15
NOx	160.9	200	161.6	162.0	0.55

Sample System Leak Check

Campic Clock		
Run#	in. of mercury	in. of mercury
	(Intial)	(Final)
multipoint	21.0	21.0
C-3	20.0	20.0
C-6	21.0	21.0
C-7	20.5	20.5
C-9	21.5	21.5
C-16	20.5	20.5
C-19	22.0	22.0
C-28	21.0	21.0
C-30 (S.S. A)	21.0	21.0
C-30 (S.S. B)	22.0	22.0

Quality Assurance Worksheet:

										Trans
	CERTIFIEI	O GAS	INITIAL CA	LIBRATION		ZERO ar	nd SPAN		ZERO ar	nd SPAN
	INPUT	i	& LINEARI	TY CHECK	TEST	CALIBRATI	ON CHECK	TEST	CALIBRATI	ON CHECK
	Concentration	Target	Initial	Difference	RUN	Final	Drift	RUN	Final	Drift
	(% or ppm)	(% Chart)	(% Chart)	(% Chart)	C-1	(% Chart)	(% Chart)	C-2	(% Chart)	(% Chart)
NOx					Avg. ppm			Avg. ppm		.3
zero	0.00	2.0	2.0	0.0	24.0	2.0	0.0	25.0	2.0	0.0
low	19.70	11.9	11.5	-0.4	% Chart			% Chart		1
mid	41.13	22.6	22.0	-0.6	14.0			14.5		ĺ
high	160.90	82.5	83.0	0.5		82.8	0.3		83.0	0.5
full scale_	200.00	,			200.0			200.0		
O2					Avg.%			Avg.%		
zero	0.00	10.0	10.0	0.0	16.63	10.0	0.0	16.63	10.0	0.0
low	4.03	26.1	25.2	-0.9	% Chart			% Chart		
mid	7.90	41.6	42.0	0.4						
high	18.10	82.4	82.6	0.2	76.5	82.4	0.0	76.5	82.2	-0.2
full scale	25.00				25.0			25.0		
CO					Avg. ppm			Avg. ppm		
zero	0.00	5.0	5.0	0.0	47.0	5.0	0.0	44.0	5.0	0.0
low	40.17	13.0	12.8	-0.2						
mid	79.71	20.9	20.0	-0.9	% Chart	84.7	0.0	% Chart	84.8	0.1
high	404.00	85.8	85.2	-0.6	52.0			49.0		
full scale	500.00				100.0			100.0		
CO2			1		Avg.%			Avg.%		ł
zero	0.00	2.0	2.0	0.0	2.40	1.5	-0.5	2.50	2.2	0.2
low	3.22	18.1	18.0	-0.1	% Chart	18.2	0.1	% Chart	17.8	-0.3
mid	8.07	42.4	42.0	-0.4						j
high	18.05	92.3	92.0	-0.3	14.0			14.5		
full scale	20.00				20.0			20.0		

	CERTIFIE) GAS		ZERO ar	nd SPAN		ZERO ai	nd SPAN		ZERO a	nd SPAN
İ	INPUT		TEST	CALIBRATI	ON CHECK	TEST	CALIBRATI	ON CHECK	TEST	CALIBRATI	ON CHECK
1	Concentration	Target	RUN	Final	Drift	RUN	Final	Drift	RUN	Final	Drift
	(% or ppm)	(% Chart)	C-3	(% Chart)	(% Chart)	C-4	(% Chart)	(% Chart)	C-5	(% Chart)	(% Chart)
NOx			Avg. ppm	•		Avg. ppm			Avg. ppm		
zero	0.00	2.0	25.0	2.0	0.0	27.0	2.0	0.0	27.0	2.5	0.5
low	19.70	11.9	% Chart			% Chart			% Chart		
mid	41.13	22.6	14.5			15.5			15.5		
high	160.90	82.5		82.5	0.0		82.2	-0.3		82.2	-0.3
full scale	200.00		200.0			200.0	<u> </u>		200.0		
O2			Avg.%			Avg.%			Avg.%		
zero	0.00	10.0	16.65	10.0	0.0	16.18	10.0	0.0	16.18	10.0	0.0
low	4.03	26.1	% Chart			% Chart			% Chart		
mid	7.90	41.6									
high	18.10	82.4	76.6	82.3	-0.1	74.7	82.4	0.0	74.7	82.5	0.1
full scale	25.00		25.0			25.0	<u> </u>		25.0		
co			Avg. ppm			Avg. ppm			Avg. ppm		
zero	0.00	5.0	47.0	5.0	0.0	20.0	5.0	0.0	19.5	5.0	0.0
low	40.17	13.0									
mid	79.71	20.9	% Chart	84.7	0.0	% Chart	84.8	0.1	% Chart	84.8	0.1
high	404.00	85.8	52.0			25.0			24.5		
full scale	500.00		100.0			100.0			100.0		.=.
CO2			Avg.%			Avg.%			Avg.%		
zero	0.00	2.0	2.50	2.2	0.2	2.70	1.8	-0.2	2.70	2.1	0.1
low	3.22	18.1	% Chart	17.5	-0.6	% Chart	17.8	-0.3	% Chart	18.1	0.0
mid	8.07	42.4									
high	18.05	92.3	14.5			15.5			15.5		
full scale	20.00		20.0	•		20.0			20.0	L	

	CERTIFIE	O GAS		ZERO ar	nd SPAN		ZERO ar	d SPAN	-	ZERO an	d SPAN
	INPUT	·	TEST	CALIBRATI	ON CHECK	TEST	CALIBRATI	ON CHECK	TEST	CALIBRATI	ON CHECK
	Concentration	Target	RUN	Final	Drift	RUN	Final	Drift	RUN	Final	Drift
	(% or ppm)	(% Chart)	C-6	(% Chart)	(% Chart)	C-7	(% Chart)	(% Chart)	C-8	(% Chart)	(% Chart)
NOx			Avg. ppm			Avg. ppm			Avg. ppm		
zero	0.00	2.0	27.0	2.4	0.4	30.0	2.2	0.2	30.0	2.0	0.0
low	19.70	11.9	% Chart			% Chart			% Chart		
mid	41.13	22.6	15.5			17.0			17.0		
high	160.90	82.5		82.8	0.3		82.9	0.5		84.0	1.6
full scale	200.00	j	200.0			200.0			200.0		
O2			Avg.%			Avg.%			Avg.%		
zero	0.00	10.0	16.18	10.0	0.0	15.50	10.0	0.0	15.50	10.1	0.1
low	4.03	26.1	% Chart			% Chart			% Chart		
mid	7.90	41.6									
high	18.10	82.4	74.7	82.3	-0.1	72.0	82.6	0.2	72.0	82.4	0.0
full scale	25.00		25.0			25.0			25.0		
CO			Avg. ppm			Avg. ppm	ļ		Avg. ppm		
zero	0.00	5.0	20.0	5.2	0.2	19.5	5.0	0.0	6.5	5.0	0.0
low	40.17	13.0		ł							
mid	79.71	20.9	% Chart	84.6	-0.1	% Chart	84.5	-0.2	% Chart	84.7	0.0
high	404.00	85.8	25.0			24.5			11.5		
full scale	500.00		100.0	-		100.0	ļ		100.0		
CO2			Avg.%			Avg.%		_	Avg.%		
zero	0.00	2.0	2.70	2.0	0.0	3.16	2.4	0.4	2.90	2.0	0.0
low	3.22	18.1	% Chart	18	-0.1	% Chart	17.4	-0.7	% Chart	17	-1.1
mid	8.07	42.4									
high	18.05	92.3	15.5			17.8		ļ	16.5		
full scale	20.00		20.0			20.0		j.	20.0		

	CERTIFIEI	O GAS		ZERO ar	nd SPAN		ZERO ar	nd SPAN		ZERO ar	d SPAN
	INPUT		TEST	CALIBRATI	ON CHECK	TEST	CALIBRATI	ON CHECK	TEST	CALIBRATI	ON CHECK
	Concentration	Target	RUN	Final	Drift	RUN	Final	Drift	RUN	Final	Drift
	(% or ppm)	(% Chart)	C-9	(% Chart)	(% Chart)	C-10	(% Chart)	(% Chart)	C-11	(% Chart)	(% Chart)
NOx			Avg. ppm			Avg. ppm			Avg. ppm		
zero	0.00	2.0	31.0	2.1	0.1	28.0	2.0	0.0	28.0	2.2	0.2
low	19.70	11.9	% Chart			% Chart			% Chart		
mid	41.13	22.6	17.5			16.0			16.0		
high	160.90	82.5		83.0	0.5		82.8	0.3		83.2	0.8
full scale	200.00		200.0			200.0			200.0		
O2			Avg.%			Avg.%			Avg.%		
zero	0.00	10.0	15.50	10.1	0.1	16.00	10.1	0.1	16.00	10.1	0.1
low	4.03	26.1	% Chart			% Chart			% Chart		
mid	7.90	41.6			•						
high	18.10	82.4	72.0	82.4	0.0	74.0	82.3	-0.1	74.0	82	-0.4
full scale	25.00		25.0			25.0			25.0		
CO			Avg. ppm			Avg. ppm			Avg. ppm		
zero	0.00	5.0	6.0	5.0	0.0	15.0	5.0	0.0	14.0	5.0	0.0
low	40.17	13.0									
mid	79.71	20.9	% Chart	84.5	-0.2	% Chart	84.3	-0.4	% Chart	84.4	-0.3
high	404.00	85.8	11.0			20.0	ļ		19.0		
full scale	500.00		100.0			100.0			100.0	ļ	
CO2		İ	Avg.%			Avg.%			Avg.%		
zero	0.00	2.0	2.90	2.0	0.0	2.80	2.0	0.0	2.80	2.2	0.2
low	3.22	18.1	% Chart	17	-1.1	% Chart	18	-0.1	% Chart	17.5	-0.6
mid	8.07	42.4									
high	18.05	92.3	16.5			16.0			16.0		
full scale	20.00		20.0			20.0			20.0		

	CERTIFIED	GAS		ZERO ar	nd SPAN		ZERO aı	nd SPAN		ZERO ar	nd SPAN
	INPUT		TEST	CALIBRATI	t	TEST	CALIBRATI	÷	TEST	CALIBRATI	ON CHECK
	Concentration	Target	RUN	Final	Drift	RUN	Final	Drift	RUN	Final	Drift
	(% or ppm)	(% Chart)	C-12	(% Chart)	(% Chart)	C-13 (TO)	(% Chart)	(% Chart)	C-13 (JF)	(% Chart)	(% Chart)
NOx			Avg. ppm			Avg. ppm			Avg. ppm		
zero	0.00	2.0	27.6	2.1	0.1	28.0	2.1	0.1	32.0	2.1	0.1
low	19.70	11.9	% Chart			% Chart			% Chart	,	
mid	41.13	22.6	15.8			16.0			18.0		
high	160.90	82.5		83.0	0.5		83.2	0.8		83.2	0.8
full scale	200.00		200.0			200.0		ŀ	200.0		
O2		-	Avg.%	}		Avg.%			Avg.%		
zero	0.00	10.0	16.00	10.0	0.0	15.50	10.0	0.0	14.20	10.0	0.0
low	4.03	26.1	% Chart			% Chart	:	[% Chart		
mid	7.90	41.6									
high	18.10	82.4	74.0	82	-0.4	72.0	82.3	-0.1	66.8	82.3	-0.1
full scale	25.00		25.0			25.0			25.0		
CO			Avg. ppm			Avg. ppm			Avg. ppm		
zero	0.00	5.0	14.5	5.0	0.0	4.0	5.1	0.1	6.0	5.1	0.1
low	40.17	13.0									
mid	79.71	20.9	% Chart	84.4	-0.3	% Chart	84.5	-0.2	% Chart	84.5	-0.2
high	404.00	85.8	19.5			9.0			11.0		
full scale	500.00		100.0			100.0	ļ		100.0		
CO2			Avg.%			Avg.%			Avg.%		
zero	0.00	2.0	2.80	2.0	0.0	3.10	2.5	0.5	3.80	2.5	0.5
low	3.22	18.1	% Chart	18	-0.1	% Chart	17.5	-0.6	% Chart	17.5	-0.6
mid	8.07	42.4	·		ļ		ľ				
high	18.05	92.3	16.0	1		17.5	ļ	ļ	27.3		
full scale	20.00		20.0			20.0			15.0		

	CERTIFIED GAS			ZERO and SPAN			ZERO and SPAN	
	INPUT		TEST	CALIBRATION CHECK		TEST	CALIBRATI	ON CHECK
	Concentration	Target	RUN	Final	Drift	RUN	Final	Drift
	(% or ppm)	(% Chart)	C-14 (TO)	(% Chart)	(% Chart)	C-14 (JF)	(% Chart)	(% Chart)
NOx			Avg. ppm			Avg. ppm		
zero	0.00	2.0	28.0	2.2	0.2	32.0	2.2	0.2
low	19.70	11.9	% Chart			% Chart		
mid	41.13	22.6	16.0			18.0		
high	160.90	82.5		83.0	0.5		83.0	0.5
full scale	200.00		200.0			200.0	ŀ	
O2			Avg.%			Avg.%		
zero	0.00	10.0	15.50	10.0	0.0	14.25	10.0	0.0
low	4.03	26.1	% Chart			% Chart		
mid	7.90	41.6						
high	18.10	82.4	72.0	82.0	-0.4	67.0	82.0	-0.4
full scale	25.00		25.0			25.0		
CO			Avg. ppm			Avg. ppm	·	
zero	0.00	5.0	5.0	5.1	0.1	7.0	5.1	0.1
low	40.17	13.0						
mid	79.71	20.9	% Chart	84.6	-0.1	% Chart	84.6	-0.1
high	404.00	85.8	10.0			12.0	!	
full scale	500.00		100.0			100.0		
CO2			Avg.%			Avg.%		
zero	0.00	2.0	3.06	2.1	0.1	3.70	2.1	0.1
low	3.22	18.1	% Chart	18	-0.1	% Chart	18	-0.1
mid	8.07	42.4						ľ
high	18.05	92.3	17.3			20.5		
full scale	20.00		20.0			20.0		

	CERTIFIED GAS		ZERO and SPAN				ZERO ar	nd SPAN
	INPUT		TEST	CALIBRATI	ON CHECK	TEST	CALIBRATI	ON CHECK
	Concentration	Target	RUN	Final	Drift	RUN	Final	Drift
	(% or ppm)	(% Chart)	C-15 (TO)	(% Chart)	(% Chart)	C-15 (JF)	(% Chart)	(% Chart)
NOx			Avg. ppm			Avg. ppm		
zero	0.00	2.0	29.0	2.0	0.0	33.0	2.2	0.2
low	19.70	11.9	% Chart			% Chart		
mid	41.13	22.6	16.5			18.5		
hìgh	160.90	82.5		82.6	0.1		82.6	0.1
full scale	200.00		200.0			200.0		
O2			Avg.%			Avg.%		
zero	0.00	10.0	15.55	10.0	0.0	14.25	10.0	0.0
low	4.03	26.1	% Chart			% Chart		
mid	7.90	41.6						
high	18.10	82.4	72.2	82.4	0.0	67.0	82.4	0.0
full scale	25.00		25.0			25.0		
CO			Avg. ppm			Avg. ppm		
zero	0.00	5.0	5.0	5.1	0.1	7.0	5.1	0.1
low	40.17	13.0						
mid	79.71	20.9	% Chart	84.6	-0.1	% Chart	84.4	-0.3
high	404.00	85.8	10.0			12.0		
full scale	500.00		100.0			100.0		
CO2			Avg.%			Avg.%		i
zero	0.00	2.0	3.04	2.0	0.0	3.72	2.0	0.0
low	3.22	18.1	% Chart	17.9	-0.2	% Chart	17.9	-0.2
mid	8.07	42.4	}					
high	18.05	92.3	17.2			20.6		
full scale	20.00		20.0			20.0		

INTERFERENCE

RESPONSE '

TEST

Environmental Instruments Division

108 South Street Hopkinton, Massachusetts 01748 (617) 435-5321

DATE OF TEST JAN 18, 1980

ANALYZER TYPE / OAR RANGO-25PPM SERIA

SERIAL NO. 10AR - 0 14B -

TEST GAS TYPE	CONCENTRATION PPM	OUTPUT RESPONSE \$ OF SPAN
<u></u>	500	4.1 PPM 4.1%
CO2	201	L.18PM <.170
CO_2	10%	L.190m 2.1%
0,	20.9%	<.1814 <.17.

Continous Emission Analyzer Interference Response Tests

Date: 7/8/88	
Technician: KRB /MM	
Analyzer Type: Them. Environmental Analyzer Model: Model 48 6as Filter (orrelation Analyzer Serial Number: 48-23576-210 Analyzer Test Range: 0-20 ppm V	_

Test Gas		Analyzer F	Response		
Type Gas	Concentration	Concentration Pm,	% of Range	Ratio	
Air	49.189.	0. O	<u> </u>	7.000 John.	
$\frac{CO_1/O_2}{CO_1/V_2}$	1271/870	-0,2		-0.017/-0.025/-11/2	
Co. /U2.	2170/370 Dry	<u> </u>		- 0.014/-0.100 1 <u>CO Impurity</u> ?	
NOx NOx	176 ppmv 3030 ppmv	0,4 0,4		0.0001 0.0001	
502 Propune	240 ppmy	0.4		0.0005 0.002	

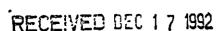
all interferences are

Response Time Data Sheet

Date:6-30)-92		
Location: _		_	
Technician:R			
Sample Manifold:	3.0	psig	••
Pump Model:	G-3 Dia	- Pump	
Sample Line Leng	gth100.	ft.	
Heat Trace Length	n <u>90'</u>	ft.	•
Condenser Design:	Jalon #5		
Analyzer Type:	N.O.x	02	
· ·	TECO 10 AR	Servomex 1400	
		0-207.	
Span Gas:	5+ack gas (TCP-3)	Stack Das (TCP-3)	
	V .		
Upscale Respon	se:		
Trial 1	. 84 min	<u>91 mm</u>	
Trial 2	. 86 min	93 min	
Trial 3	. 89 min	. 93 min	
Average .	. 86 min.	.92 min	
_	ponse:	a 3 ·	
Trial 1	. 89	mm	
Trial 2	. 86 min		
Trial 3	20 ·	<u>98 min</u>	
Average	. 88 min	<u>96 min</u>	

Comments:

APPENDIX D: EXAMPLE CALIBRATION CERTIFICATIONS





CERTIFICATE OF ANALYSIS-EPA PROTOCOL MIXTURES

CUSTOMER:

WILSON OXYGEN AND SUPPLY

REFERENCE #:

109-16269

CYLINDER #:

SX-25924

PROTOCOL:

1

CYLINDER PRESSURE: 1800

LAST ANALYSIS DATE: 12/14/92

EXPIRATION DATE:

06/14/94

REPLICATE CONCENTRATIONS

COMPONENT

NITRIC OXIDE

12/07/92 DATE:

DATE:

12/14/92

MEAN CONC

6.82 PPM

6.86 PPM

6.83PPM

6.89 PPM

/ /

6.78PPM

6.79 PPM

6.72PPM

COMPONENT

NITROGEN DIOXIDE

DATE:

DATE:

MEAN CONC

0.25 PPM

COMPONENT.

DATE:

DATE:

MEAN CONC

BALANCE GAS:

NITROGEN

REFERENCE STANDARDS

SRM #

: 2628A

CYLINDER #

: CLM-4176

CONCENTRATION: 9.75 PPM

ACCEPTED BY

WILSON OXYGEN

1650 Enterprise Parkway P.O. Box 358 Twinsburg, Ohio 44087

Phone: (216) 425-4406 Toll Free: (800) 426-9427



10-Aug-92
BIG THREE INDUSTRIES

P.O. NO.: 128072992 AUSTIN. TX

CERTIFICATION OF CYLINDER # CC-115214

COMPONENT:

NITRIC OXIDE Total NOm NITROGEN

Cylinder pressure: Expiration date:

MEAN CONCENTRATION:

19.3 +/- 1.3 ppm 19.9 ppm BALANCE

1800 psig 10-Feb-94

This mixture was prepared and analyzed following EFA Revised Traceability Protocol No.1, Section 3.0.4, per Procedure G1. The concentration of the Nitric Oxide was determined by direct comparison with NIST SRM 1683b, Sample No.:45-12-P, S/N CLM-2231, 47.6 +/- 0.7 ppm Nitric Oxide in Nitrogen, dated October 31, 1991. The analysis was performed on a Beckman 951A chemiluminescent-type analyzer measuring the reaction of Nitric Oxide with Ozone. S/N 00100508, 0-100 ppm range. The last multipoint calibration was done on August 3, 1992.

Authorized signature





10-Aug-92 BIG THREE INDUSTRIES P.O. NO.: 128072992 AUSTIN, TX

CERTIFICATION OF CYLINDER # CC-115228

COMPONENT:

NITRIC OXIDE Total NOx NITROGEN

Cylinder pressure: Expiration date:

MEAN CONCENTRATION:

41.2 +/- 1.3 ppm 42.6 ppm BALANCE

1800 psig 10-Feb-94

This mixture was prepared and analyzed following EPA Revised Traceability Protocol No.1, Section 3.0.4, per Procedure G1. The concentration of the Nitric Oxide was determined by direct comparison with NIST SRM 1683b. Sample No.:45-12-P, S/N CLM-2231, 47.6 +/- 0.7 ppm Nitric Oxide in Nitrogen, dated October 31, 1991. The analysis was performed on a Beckman 951A chemiluminescent-type analyzer measuring the reaction of Nitric Oxide with Ozone. S/N 00100508, 0-100 ppm range. The last multipoint calibration was done on August 3, 1992.

Authorized signature



1290 COMBERMERE STREET, TROY, MI 48083

(313) 589-2950 FAX: (313) 589-2134

CERTIFICATE OF ANALYSIS: EPA PROTOCOL GAS

Customer

CUBIX CORPORATION

9225 LOCKHART HWY **AUSTIN TX 78747**

Assay Laboratory

Scott Specialty Gases, Inc.

1290 Combermere Troy, MI 48083

Purchase Order JOHN

WETHEROLD

五 等一次不明的不明的人的母子是我也是我们的人人不会是我也是我们我就是我们的人的女子

以中ののとのないでは、からいことがなっているとなるない。 はるないませんとないできないが、そうないない

Scott Project # 550913

ANALYTICAL INFORMATION

Certified to exceed the minimum specifications of EPA Protocol 1 Procedure # G1, Section Number 3.0.4

Cylinder Number Cylinder Pressure

ALM005440 1900 psig ... ; Certification Date **Previous Certification Dates**

5-17-93

None

General Exp. Date 5-17-95

Acid Rain Exp. Date 11-17-94

ANALYZED CYLINDER

Components

Nitric Oxide

Certified Concentration

80.10 ppm

80.80 ppm

Analytical Uncertainty*

Reference Value Only

±1% NIST Directly Traceable

Total Oxides of Nitrogen

Balance Gas: Nitrogen

*Analytical uncertainty is inclusive of usual known error sources which at least includes reference standard error & precision of the measurement processes.

REFERENCE STANDARD

Type

Expiration Date

SRM 1684B 1-6-94 Cylinder Number

CIM002155

Concentration

95.10 ppm NO in N2

INSTRUMENTATION

Instrument/Model/Serial #

NO: Horiba/OPE-235/483814

Last Date Calibrated

4-12-93

Analytical Principle Chemiluminescence

ANALYZER READINGS (Z=Zero Gas R=Reference Gas T=Test Gas r=Correlation Coefficient)

Components

Nitric Oxide

First Triad Analysis

Date: 5-10-93

Z1=0.00

Response Units: mv T1=80.00 R1=95.10

T2=80.00

R3=95.10

R2-95.10 22=0.00 Z3-0.00 T3=80.00

Avg. Conc. of Cust. Cyl. 80.00 ppm

Second Triad Analysis Date: 5-17-93

Response Units: mv Z1=0.00 R1=95.10 T1 = 80.20T2-80.20 R2=95 10 72 = 0.00

Z3-0.00 T3=80.20 R3=95.10 Avg. Conc. of Cust. Cyl. 80.20 ppm

Calibration Curve

Concentration=A+Bx+Cx2+Dx3+Ex4

-0.99999 SRM 1684B

A=-0.000967384 Constants:

B=1.000115 C=0

E=0

Concentration=A+Bx+Cx2+Dx3+Ex4

Concentration=A+Bx+Cx²+Dx³+Ex⁴

Special Notes

If this product is used for Acid Rain Rule Compliance, the Acid Rain Expiration Date noted above applies per 40 CFR Part 75, Appendix H. Otherwise, the General Expiration Date applies.

Analyst Frank P. Doran



1290 COMBERMERE STREET, TROY, MI 48083

(313) 589-2950 FAX: (313) 589-2134

CERTIFICATE OF	ANALYSIS:	EPA PROTOCO	OL GAS

Customer CUBIX CORPORATION 9225 LOCKHART HWY AUSTIN, TX, 78747 Assay Laboratory
Scott Specialty Gases, Inc.
1290 Combernere
Troy, MI 48083

Purchase Order 93401 Scott Project # 553985

ANALYTICAL INFORMATION

Certified to exceed the minimum specifications of EPA Protocol 1 Procedure # G1, Section Number 3.0.4

Cylinder Number Cylinder Pressure ALM038818 1900 psig Certification Date

8-9-93

General Exp. Date

8-9-95

Previous Certification Dates

None

Acid Rain Exp. 🕥

8-9-95

Da

ANALYZED CYLINDER

Components Nitric Oxide Certified Concentration

160.4 ppm

Analytical Uncertainty*

±1% NIST Directly Traceable

Total Oxides of Nitrogen

160.4 ppm

Reference Value Only

Balance Gas: Nitrogen

*Analytical uncertainty is inclusive of usual known error sources which at least includes reference standard error & precision of the measurement processes.

REFERENCE STANDARD

Type CRM **Expiration Date**

3-5-97

Cylinder Number ALM024135 Concentration

244.7 PPM N0/N2

INSTRUMENTATION

Instrument/Model/Serial # NO: Beckman/951A/270-082899B Last Date Calibrated 6-21-93

Analytical Principle Chemiluminescence

ANALYZER READINGS (Z=Zero Gas R=Reference Gas T=Test Gas r=Correlation Coefficient)

Second Triad Analysis Calibration Curve First Triad Analysis Components Concentration=A+Bx+Cx+Dx3+Ex4 Nitric Oxide Date: 8-2-93 Response Units: mv Date: 8-9-93 Response Units: mv R1=97.80 T1=64.10 Z1=0.00 r=0.99999 2 SRM 1685 Z1 = 0.00R1=97.80 T1=64.10 R2=97.80 22=0.00 T2=64.10 Constants: A=0.008456338 T2=64.10 R2=97.80 72=0.00R3=97.80 B=2.502916 C=0 Z3=0.00 T3=64.10 R3=97.80 Z3=0.00 T3=64.10 Avg. Conc. of Cust. Cyl. 160.4 ppm D=0E=0 Avg. Conc. of Cust. Cyl. 160.4 ppm Concentration=A+Bx+Cx+Dx3+Ex4 ... Concentration=A+Bx+Cx+Dx3+Ex

Special Notes

If this product is used for Acid Rain Rule Compliance, the Acid Rain Expiration Date noted above applies per 40 CFR Part 75, Appendix H. Otherwise, the General Expiration Date applies.

Tim Sandesson
Analyst Tim Sanderson



1290 COMBERMERE STREET TROY, MI 48083 PHONE: (313) 589-2950 FAX NO: (313) 589-2134

CUBIX CORPORATION 9225 LOCKHART HWY AUSTIN TX 78747 -

Date: ___2/3/92

Our Project No.: 052883

Your P.O. No.: 910471

Gentlemen:

Thank you for choosing Scott for your Specialty gas needs. The analyses for the gases ordered, as reported by our laboratory, are listed below. Results are in volume percent, unless otherwise indicated.

ANALYTICAL REPORT

Analytical			Analytical
Cyl. No. ALMO18473 Accuracy	<u>+/-1%</u>	Cyl. No.AAL20862	Accuracy + / -1%
Component	Concentration	Component	Concentration
CARBON MONOXIDE	79.71ppm	CARBON MONOXI	DE 8.066ppm
METHANE	79.64ppm	METHANE	7.998ppm
BALANCE	AIR	BALANCE	AIR
ACUBLEND MASTER GAS		ACUBLEND MAST	ER GAS
1400		•	
Analytical Cyl. No. <u>ALMO16314</u> Accuracy Component		Cyl. No	Analytical Accuracy Concentration
CARBON MONOXIDE	40.17ppm		
METHANE	39.77ppm	<u> </u>	A constant
BALANCE	AIR	-	
ACUBLEND MASTER GAS			
Analyst Les Obey		Approved	Bokh
Analyst Les Company for one wi	high falls to comply with this analysi	19	the Company without extra cost

The only liability of this Company for gas which falls to comply with this analysis shall be replacement thereof by the Company without extra cost.

CERTIFIED REFERENCE MATERIALS

EPA PROTOCOL GASES

ACUBLEND®

CALIBRATION & SPECIALTY GAS MIXTURES

ACCESSORY PRODUCTS

CUSTOM ANALYTICAL SERVICES

PLUMBSTEADVILLE, PENNSYLVANIA / SAN BERNARDINO, CALIFORNIA / HOUSTON, TEXAS / WHEELING, ILLINOIS -SOUTH PLAINFIELD, NEW JERSEY: / FREMONT, CALIFORNIA / WAKEFIELD, MASSACHUSETTS / LONGMONT, COLDRADO



Shipped From:

3714 LAPAS DRIVE

HOUSTON

TX 77023

Phone: 713-644-4820

Fax: 713-644-0244

CERTIFICATE OF ANALYSIS

CUBIX CORPORATION

9225 LOCKHART HWY

PROJECT #: 04-19430

PO#: 92373

- ITEM #: 04024311 1AL

DATE: 9/01/92

AUSTIN

TX 78747

CYLINDER #: ALMO03153

ANALYTICAL ACCURACY: +/- 1%

REQUESTED GAS ANALYSIS COMPONENT CONC MOLES (MOLES) 15. PPM CARBON MONOXIDE 15. PEM 14,5 PPM METHANE AIR BAL

ANALYTICAL METHOD; GRAV. MASTER GAS

ANALYST: _

A PHILIPSTEADVILLE, PENNSYLVANIA / TROY, MICHIGAN / HOUSTON, TEXAS / DUTILATE NOT THE AROLINA SOUTH PLAINFIELD, NEW JERSEY / FREMONT, CALIFORNIA / WAKEFIELD, MASSACHUSETTS / LONGMONT, COLORADO BATON ROUGE, LOUISIANA



ALPHAGAZ

SPECIALTY GAS DIVISION

P.O. Box 1026 11426 Fairmont Pkwy. La Porte, Texas 77571 Phone (713) 474-8400 Fax (713) 474-8419 USA (800) 248-1427

25 August 1992

P.O. Number : 1280729928 AGZ Document: #1425293

Customer: BIG 3 AUSTIN

Valve Type ..: CGA 590

CERTIFICATION OF CYLINDER # CC79058

Component

MOLE %

METHANE CARBON . MONOX LDE 2.1 PPM 2.8 PPM

AIR

BALANCE

Respectification date: 25 August 1993

Prepared By:

Mary Vayne



Scott Specialty Gases, Inc.

3714 LAPAS DRIVE, HOUSTON, TX 77023-0000 PHONE: 713-644-4820 FAX:713-644-0244

10/14/91

CUBIX CORPORATION 9225 LOCKHART HWY

PROJECT #: 04-13615

PO #: 910471

AUSTIN

TX 78747-0000

CYLINDER #: AAL13947

ANALYTICAL ACCURACY: +-1%

REQUESTED

ANALYSIS : (MOLES) U/M

COMPONENT

CONCENTRATION

PCT

ARBON DIOXIDE GEN

ROGEN

3.2 PCT FOT 18.0 BALANCE

POT 18.10 BALANCE

NOTES:

ANALYTICAL METHOD: ACUBLEND MASTER



Scott Specialty Gases, Inc.

3714 LAPAS DRIVE, HOUSTON, TX 77023-0000

10/14/91

PHONE: 713-644-4820 FAX:713-644-0244

CUBIX CORPORATION 9225 LOCKHART HWY

PROJECT #: 04-13615

20 =: 910471

AUSTIN

TX 78747-0000

CYLINDER #: AAL268

ANALYTICAL ACCURACY: +-1%

COMPONENT

REQUESTED

, ANALYSIS 1

(MOLES) U/M

REON DIOXIDE

OGEN

CONCENTRATION

POT 8.07

0.8 8.0

PCT

7.90 FCT

BALANCE

BALANCE

NOTES:

ANALYTICAL METHÓD: ACUBLEND MASTER

APPROVED BY: ____

PLUMSTEADVILLE, PENNSYLVANIA / TROY, MICHIGAN / HOUSTON, TEXAS / DURHAM, NORTH CAROLINA SOUTH PLAINFIELD, NEW JERSEY / FREMONT, CALIFORNIA / WAKEFIELD, MASSACHUSETTS / LONGMONT, COLORADO BATON ROUGE, LOUISIANA



Scott Specialty Gases, Inc.

3714 LAPAS DRIVE, HOUSTON, TX 77023-0000 PHONE: 713-644-4820 FAX:713-644-0244

10/14/91

CUBIX CORPORATION

PROJECT #: 04-13615

9225 LOCKHART HWY

PO #: 910471

AUSTIN

TX 78747-0000

CYLINDER #: AAL20488

ANALYTICAL ACCURACY: +-1%

REQUESTED CONCENTRATION

ANALYSIS T (MOLES) U/M

COMPONENT

PCT

CARBON DIOXIDE

PCT 18.0 4.0 PCT

18.05 _4.03 PCT

YGEN TROGEN

BALANCE

BALANCE

NOTES:

ANALYTICAL METHOD: ACUBLEND MASTER

APPROVED BY:

APPENDIX E: PROPOSED TEST SCHEDULE

TEST SCHEDULE NOT DETERMINED YET

APPENDIX F: PLOT PLAN, STACK DIAGRAM STACK TRAVERSE LAY-OUTS

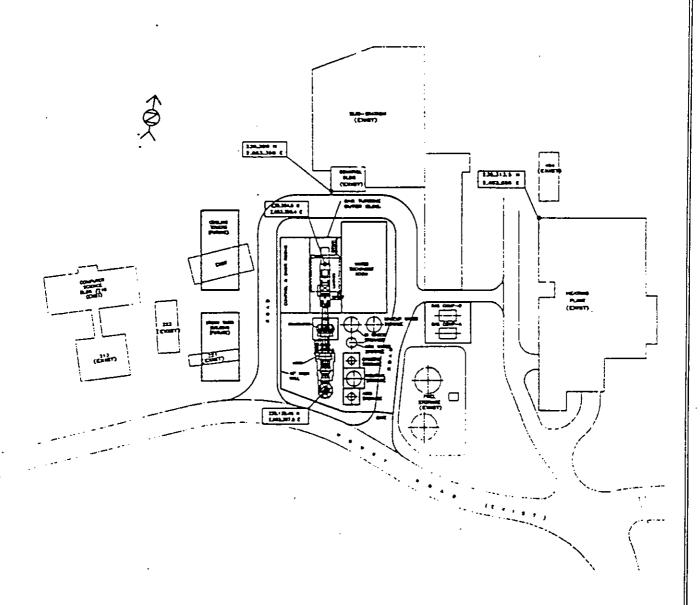


Figure 5. Site Plan of the University of Florida Co-Generation Unit



Figure 10.- 6. 4 - 3" Dia. Test ports with 9" nipples o Stack Height spaced equally @ 90 Deg 6 92 - 6 15' - 0" Platform height with top rail 3' - 6' above Stack sampling port location University of Florida Co-Gen Unit Distanca to first obstruction is 29' - 0" 7.75 Top of heat recovery unit entry point PALET AND PILTER Q 41'-# +/-B. 30-8-/-) Description



EAST ELEVATION

Circular Stack Sampling Traverse Point Layout (EPA Method 1)

Date:			Port E Stack Stack Total No. of No. of	Port + Stack ID:in. Port Extension:9in. Stack ID:117in. Stack Area:74.66ft^2 Total Req'd Traverse Points:44 No. of Traverse Points:22/diam. No. of Traverse Points:22/port		
Stack Diagram (Side View showing major unit components, dimensions and nearest upstream and downstream disturbances)						
Traverse		 -			Distance	
Point		Length (% of di		San San San San San San San San San San	from Reference	
Number	Numbe	r of trave	-	s/diam.	Point (inches)	
	4	6	8	22		
1 2 3 4 5 6 7 8 9 10 11 12	6.7 25.0 75.0 93.3	4.4 14.6 29.6 70.4 85.4 95.6	3.2 10.5 19.4 32.3 67.7 80.6 89.5 96.8	1.1 3.5 6.0 8.7 11.6 14.6 18.0 21.8 26.2 31.5 39.3 60.7 68.5 73.8 78.2 82.0 85.4 88.4 91.3 94.0 96.5 98.9	10.29 13.10 16.02 19.18 22.57 26.08 30.06 34.51 39.65 45.86 54.98 80.02 89.15 95.35 100.05 104.94 108.92 112.43 115.82 118.98 121.91 124.71	

Table 4 University of Florida Co-Generation Data

Address:

Mowry Road, Building No. 82 University of Florida Gainesville, Florida

Unit Description:

One Combustion Turbine(CT) and one Heat Recovery Steam Generator(HRSG) is under construction at this site.

The CT unit is a General Electric Model LM 6000 and fired by natural gas with steam injection for NO_x control to 25 PPMVD at 15% oxygen.

The CT is rated at 43.3 MW on natural gas.

The HRSG unit operates on the CT exhaust gases and is supplementally fired on natural gas using duct burners to generate steam only.

Exhaust Stack Information:

Height:

93 Ft.

Diameter:

9.75 Ft. (Round stack)

Gas Flow:

325,200 ACFM

Velocity

72.6 FPS

Exit Temp.:

257 $^{\rm o}$ F (combine output of both CT & HRSG units)

Drawings:

The location of the site is shown in Figure 4.

The site layout is shown in Figure 5.

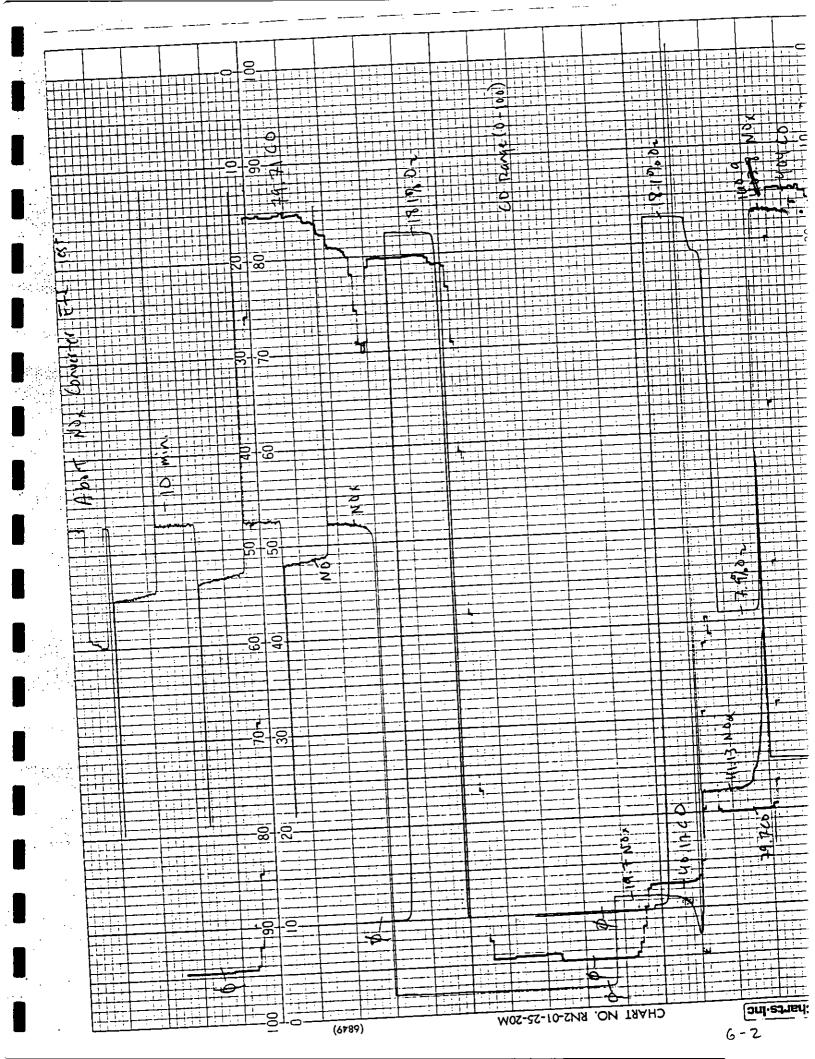
The exhaust stack test port location is shown in Figure 6.

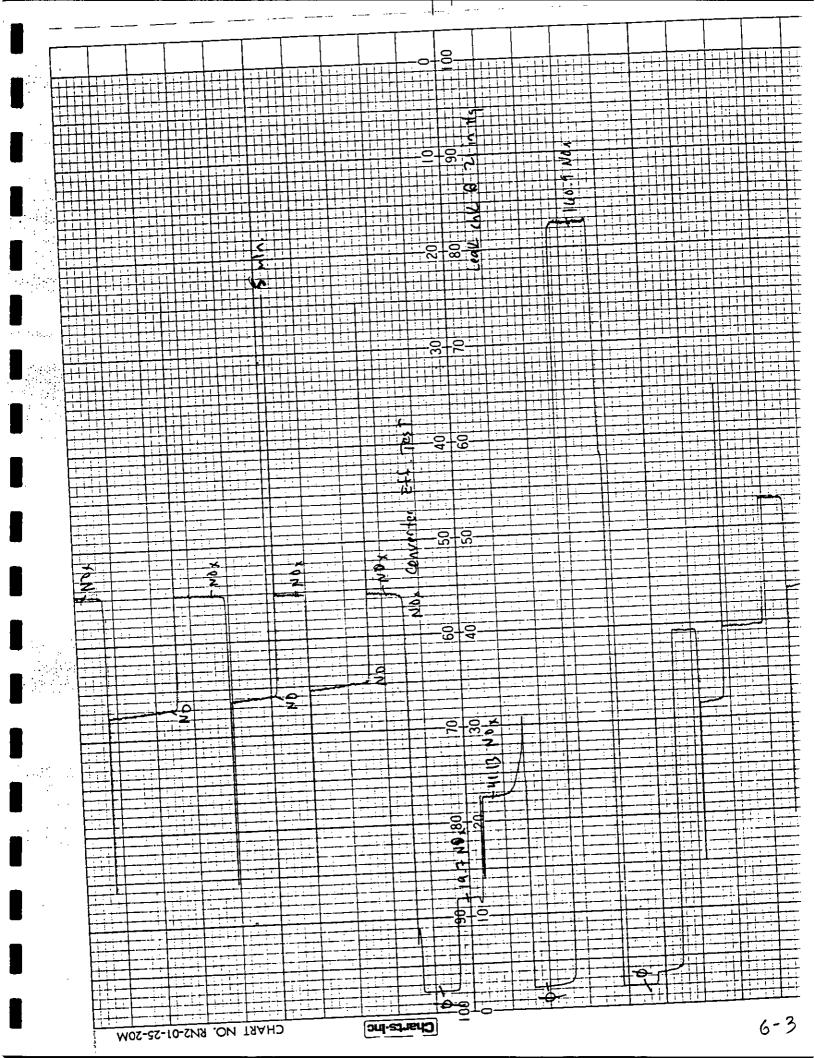
Authorized Air Permit:

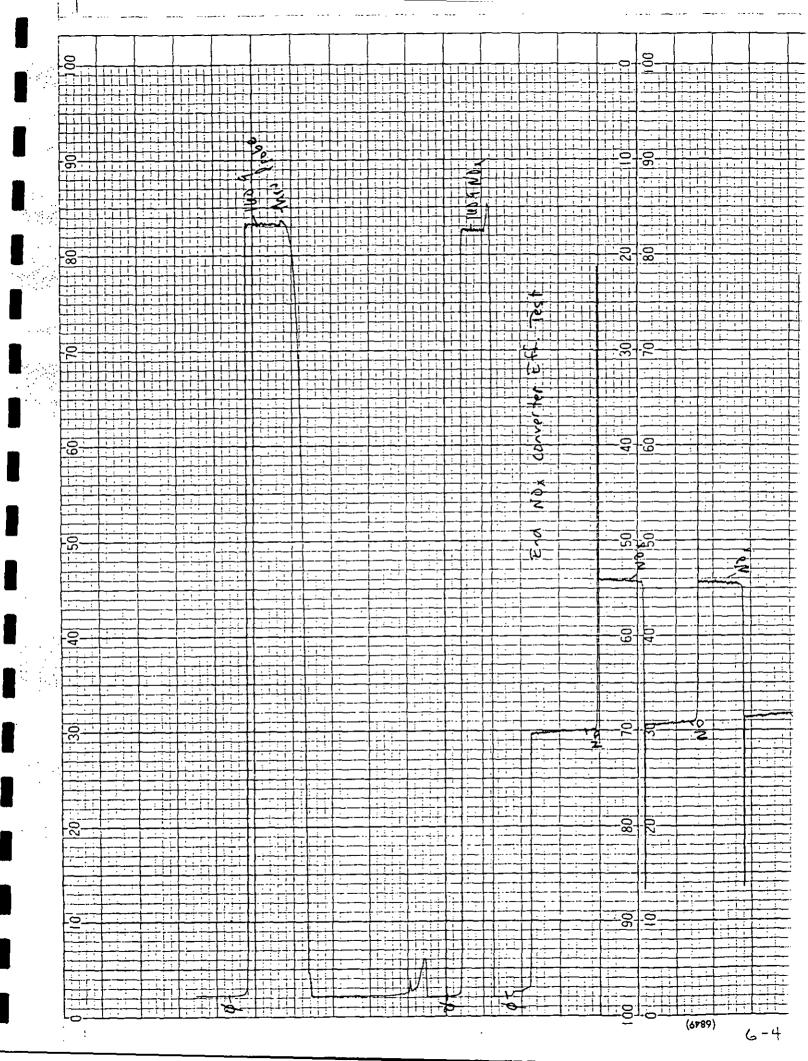
The Florida Department of Environmental Regulation (FDER) Air Construction Permit No. is AC 01-204652.

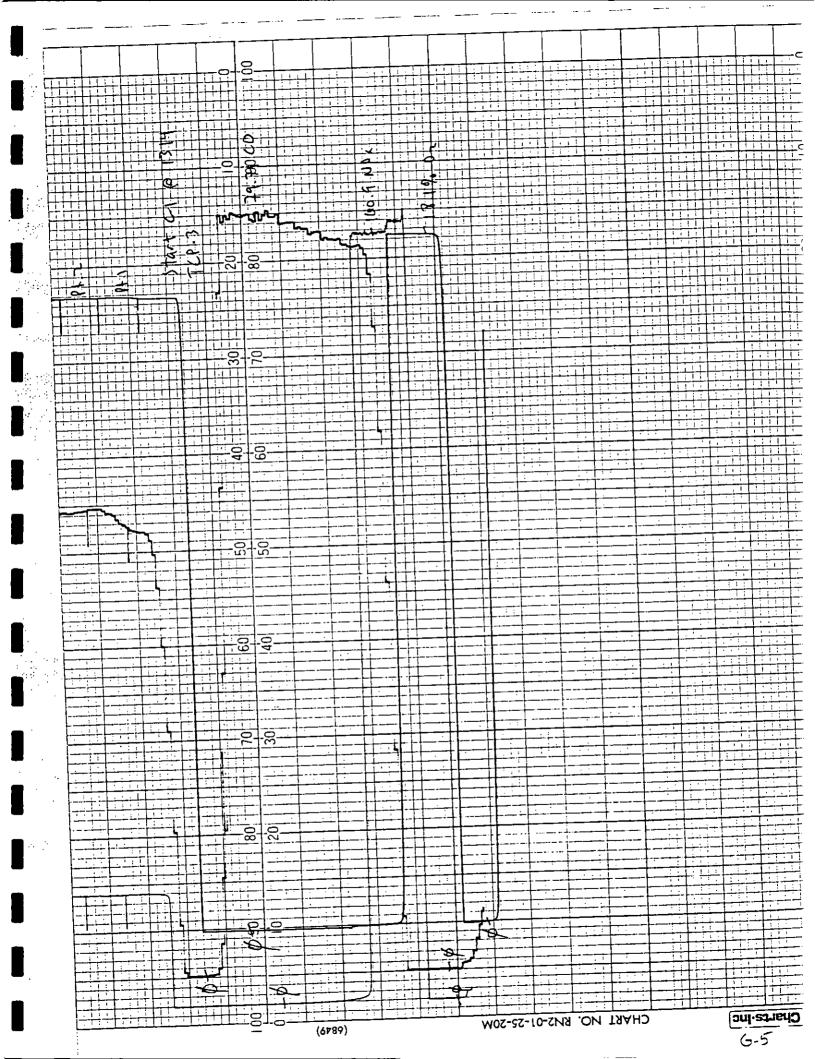
APPENDIX G: EXAMPLE STRIP CHART RECORDS

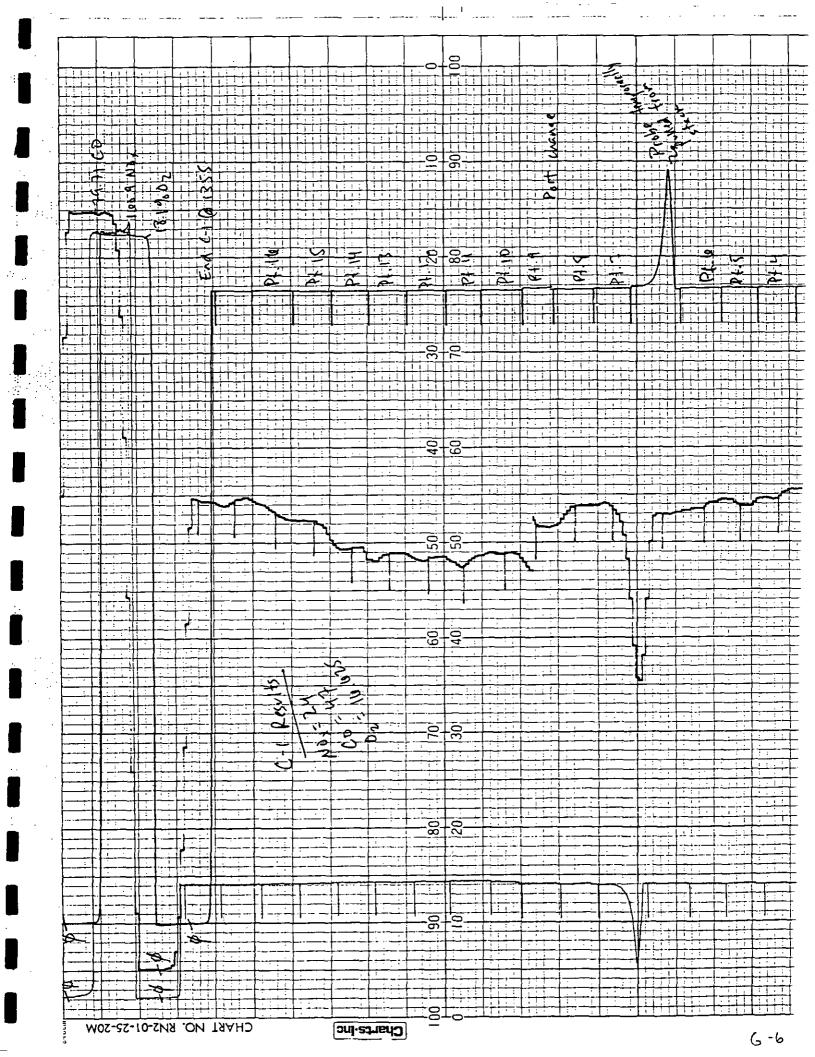
NOX, CO, O2

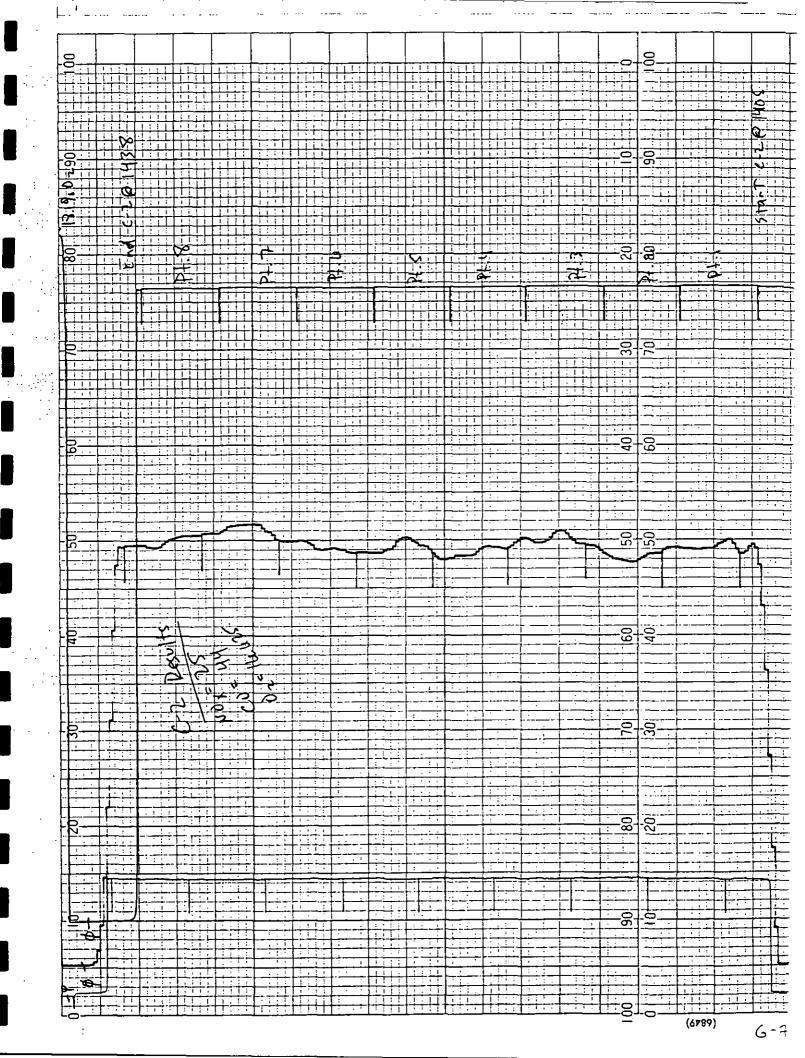


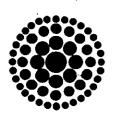


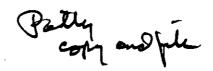












Florida Power

RECEIVED

DEC - 9 1993

Division of Air Resources Management

December 3, 1993

Mr. Chris Kirts Air Program Manager, Northeast District 7825 Bay Meadows Way Suite B200 Jacksonville, Florida 32256

Dear Mr. Kirts:

Re: Initial Startup of New Combustion Turbine at the University of Florida DEP Permit No. AC01-204652

As required by 40 CFR 60, Florida Power Corporation (FPC) is providing the Department of Environmental Protection (DEP) notification of the initial startup of the new combustion turbine at FPC's University of Florida Cogeneration facility. The initial startup is scheduled for December 17, 1993. FPC will subsequently notify your agency of the actual date that startup occurred.

Please feel free to contact me at (813) 866-5158 if you have any questions or if you need additional information.

Sincerely,

Scott H. Osbourn

Senior Environmental Engineer

cc: Mr. John Brown, DEP Tallahassee