Florida Electrical Power Plant Siting Act

Site Certification Application Volume 3 of 3 Treasure Coast Energy Center



Submitted by: Florida Municipal Power Agency April 2005





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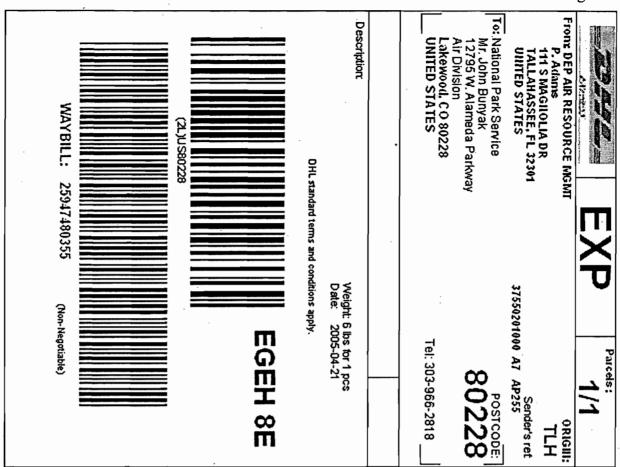
Cc: Graziani, Darrel; Mulkey, Cindy; Linero, Alvaro

Subject: PSD-FL-353, 1110121-001-AC, Treasure Coast Energy Center

The Bureau of Air Regulation is transmitting to you by this email an electronic version of a PSD application submitted by the Florida Municipal Power Agency (FMPA) for construction of the Treasure Coast Energy Center in Fort Pierce, St. Lucie County, Florida.

Your comments may be forwarded to Al Linero at the Bureau of Air Regulation or faxed to 850-921-9533. If you have any questions, please contact Cindy Mulkey, review engineer, at 850-921-8968.

Sincerely, Patty Adams 850-921-9505



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1.0 Introduction

The Florida Municipal Power Agency (FMPA) proposes to install a 1x1 F-Class Combined Cycle Unit and associated support facilities (Project) at the new Treasure Coast Energy Center (hereinafter referred to as the Energy Center), near Fort Pierce, St. Lucie County, Florida. The Energy Center will include a 1x1 combined cycle unit (Unit 1) which will include a combustion turbine generator (CTG), a duct-fired heat recovery steam generator (HRSG), and a steam turbine generator (STG), operating at a nominal rating of 300 MW. New major support facilities include an approximately 990,000 gallon fuel oil storage tank, a natural gas fired auxiliary boiler, a diesel engine driven fire pump and associated 500 gallon fuel oil storage tank, a safe shutdown generator and a mechanical draft cooling tower.

This report is a technical support document for the Prevention of Significant Deterioration Air Permit Application. The following sections contain a project characterization, best available control technology (BACT) determination, air quality impact analysis (AQIA), and additional impact analyses designed to provide a basis for the Florida Department of Environmental Protection's (FDEP) preparation of an air construction permit for the Project.

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2.0 Project Characterization

The following sections briefly characterize the Project, including a general description of the location, facility, and emission units, as well as a summary of the estimated emissions and a discussion of New Source Review (NSR) applicability and a regulatory review.

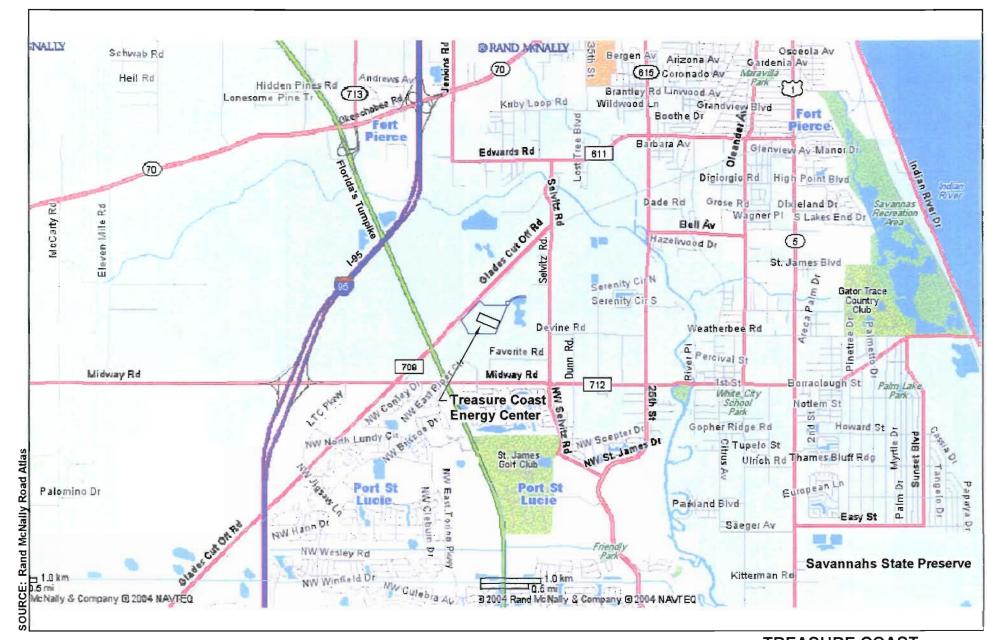
2.1 Project Location

The Project is located in St. Lucie County, Southwest of the City of Fort Pierce. Figure 2-1 shows the general location of the Project. The approximate UTM coordinates of the site are 561,516.1 m East and 3,028,996.3 m North (Zone 17). The nearest Federal Prevention of Significant Deterioration (PSD) Class I Area is the Everglades National Park (ENP), located approximately 180 km Southwest of the Project site. The Chassahowitzka class 1 area is approximately 260 km Northwest of the Project site. The topography of the area is unpronounced and considered relatively flat.

2.2 Project Description

The Project installation will be a 1x1 F-Class Combined Cycle Unit (Unit 1) which will include a combustion turbine generator (CTG), a duct-fired heat recovery steam generator (HRSG), and a steam turbine generator (STG). Unit 1 will have a nominal rating of 300 MW. New major support facilities include an approximately 990,000 gallon fuel oil storage tank, a natural gas fired auxiliary boiler, a diesel engine driven fire pump with an associated 500 gallon fuel oil storage tank, a safe shutdown generator with an associated 1,000 gallon fuel oil storage tank, and a mechanical draft cooling tower.

Unit 1 will be dual fueled with natural gas as the primary fuel and ultra-low sulfur (ULS) fuel oil (0.0015 percent sulfur) as an alternate fuel. The CTG will have an evaporative cooler to increase warm weather power generation by increasing the CTG inlet air density. Power augmentation systems for the CTG are not included. The CTG will be designed to operate in a pseudo simple cycle mode where the steam from the HRSG bypasses the steam turbine and is dumped to the condenser. Air emissions when operating in this pseudo-simple cycle mode are expected to be no different then the air emissions when operating in typical combined cycle mode operation, as the combustion gases will still pass through the HRSG and the SCR will still be used for control of NO_x emissions.









TREASURE COAST ENERGY CENTER PROPOSED PROJECT LOCATION FIGURE 2-1

2.2.1 Combustion Turbine Generator (CTG)

The PSD application is based on a General Electric PG7241 FA enhanced combustion turbine generator with modulating inlet guide vanes installed outdoors. The combustion turbine generator unit will include the following major features:

- Dual fuel firing system using natural gas or ULS fuel oil.
- Dry low NO_x combustion system for natural gas firing.
- Direct connected generator with static excitation.
- Acoustic enclosure for turbine.
- Self cleaning inlet air filter system with silencers and evaporative coolers.
- Lube oil systems.
- Static starting system.
- Water injection system for NO_x reduction when firing fuel oil.
- Fire detection/carbon dioxide fire protection systems.
- Mark VI control system.
- Off-line/on-line water wash system.
- Package Electrical and Electronics Control Compartment.

2.2.2 Heat Recovery Steam Generator (HRSG)

The HRSG will convert waste heat from the CTG exhaust to steam for use in driving the STG. The HRSG is expected to be a natural circulation, three pressure, reheat unit with supplemental duct firing by natural gas only to maximize unit output. Selective catalytic reduction (SCR) for NO_x control is included. The HRSG will discharge to a metal exhaust stack approximately 170 feet tall. A stack damper will be included to minimize heat loss during unit shutdowns.

2.2.3 Steam Turbine Generator (STG)

The STG is expected to be a tandem-compound single reheat condensing turbine operating at 3,600 rpm. The steam turbine will have one high pressure section with a nominal 1,800 psig throttle pressure, one intermediate pressure section, and one low pressure section. Turbine suppliers' standard auxiliary equipment, lubricating oil system, hydraulic oil system, and supervisory, monitoring and control systems are included. A surface condenser is included for condensing steam from the turbine exhaust and will utilize a recirculating cooling tower system for cooling. A single synchronous generator is included which will be direct coupled to the steam turbine. Generator suppliers' standard auxiliary equipment, supervisory, monitoring, and control systems, and static excitation system are included.

A 5,000 pounds per hour natural gas fired auxiliary boiler will be included to provide steam for the STG steam seal system during startups.

2.2.4 Cooling Tower

A multiple cell, mechanical draft, counterflow cooling tower will be used for plant cooling. The cooling tower will be of fiberglass construction and installed on a reinforced concrete basin which will include a pump intake structure housing the two 50 percent capacity circulating water pumps and one 100 percent capacity auxiliary cooling water pump. Circulating water chemical feed system will be included. Makeup water to the cooling tower is expected to be from treated sewage plant effluent (reclaimed water). Provisions will be included to utilize municipal water and groundwater as emergency sources of cooling tower makeup. The cooling tower will be equipped with drift eliminators with a design drift rate of 0.0005 percent of the circulating water flow rate.

2.2.5 Mode of Operation

Unit 1 is designed for unlimited operation on natural gas and up to 500 hours per year of operation with ULS fuel oil, including an unlimited number of starts annually. A maximum of approximately 300 starts are expected annually, with an expected breakdown of 50 cold starts, 200 warm starts and 50 hot starts.

2.2.6 Fuel

The fuel for Unit 1 will be natural gas and ULS (0.0015 percent sulfur) fuel oil. Natural gas will be delivered to the site by existing and new pipelines from Florida Gas Transmission (FGT). Fuel oil delivery will be by truck. Fuel oil storage of slightly less than one million gallons will be provided to allow full load operation for approximately 3 days. A truck unloading and transfer station will be installed. The fuel oil tank will be installed within a dike area to provide containment. A foam fire suppression system will be installed on the fuel oil tank. This application is for unlimited operation on natural gas and up to 500 hours per year of operation with ULS fuel oil.

2.2.7 Air Quality Control

The Project is a prevention of significant deterioration (PSD) major source. Based on the BACT analysis, emission control for NO_x will be by the use of combustion turbine dry low NO_x burners and SCR when firing natural gas or water injection and SCR when firing ULS fuel oil. Control of other pollutants will be by good combustion control and use of natural gas and ULS fuel oil.

2.3 Project Emissions

This section discusses the potential to emit (PTE) of all regulated PSD air pollutants resulting from the Project. Emissions from the Project will be generated from the following emissions units:

- One General Electric CCCT/HRSG with supplemental duct firing (Unit 1).
- One natural gas fired auxiliary boiler.
- One diesel engine driven fire pump with associated 500 gallon fuel oil storage tank.
- One safe shutdown generator with associated 1,000 gallon fuel oil storage tank.
- One approximately 990,000 gallon fuel oil storage tank.
- One mechanical draft cooling tower.

The emission calculations for each of these emission units are shown in Appendix A. The following sections briefly describe the basis for the emission calculations.

2.3.1 Unit 1 Emissions

Performance data for Unit 1 at loads of 40, 50, 75, and 100 percent, natural gas or distillate fuel oil firing, and ambient air temperatures of 26° F, 59° F, 73° F, and 100° F are provided in Appendix A.

Ambient temperature data were selected based on meteorological data from St. Lucie County, Florida. An ambient temperature of 26° F represents the winter seasonal site minimum temperature and corresponds to maximum heat input and power generation. An ambient temperature of 73° F represents the average annual site temperature, which is representative of the average heat input rate. An ambient temperature of 100° F represents the summer seasonal maximum site temperature and corresponds to the lowest heat input rate for the combustion turbine. An ambient temperature of 59° F represents ISO conditions.

The maximum pound per hour emission rates (rounded to the nearest tenth of a pound) considering all ambient temperatures are presented in Table 2-1.

2.3.2 Natural Gas Auxiliary Boiler

The natural gas auxiliary boiler will be capable of firing natural gas only. The auxiliary boiler will have a heat input rate of approximately 7.2 mmBtu/h. The potential emissions from this emissions unit are based on unlimited operation. Projected emissions from the auxiliary boiler are based on vendor data representative of the type and size of the unit to be installed.

Table 2-1 CTG/HRSG Maximum Emission Rates (lb/h)*								
Pollutant	Natural Gas Firing (lb/h)	Distillate Oil Firing (lb/h)						
NO _x	17.5	81.1						
SO_2	13.6	6.3						
CO	52.3	92.4						
PM/PM ₁₀ (front half only)	14.7	22.5						
PM/PM ₁₀ ** (front and back half)	38.0	52.0						
VOC	5.1	10.2						
SAM	6.1	3.5						

^{*}Maximum pound per hour emission rates (rounded to the nearest tenth of a pound) for the CCCT with duct firing considering site ambient temperatures and partial load operation.

2.3.3 Diesel Engine Fire Pump

The diesel engine fire pump is considered emergency equipment and as such is considered exempt from permitting in accordance with Rule 62-210.300(3). This is discussed further in Section 2.6.3. While this emissions unit is exempt from permitting, its' emissions are still included in the potential to emit for the Project and in the AQIA. The diesel engine fire pump will fire ULS fuel oil. In determining the potential annual emissions, based on National Fire Protection Association (NFPA) guidelines it is conservatively estimated that the diesel engine fire pump will operate approximately 200 hours per year. Projected emissions from the diesel engine fire pump are based on vendor data representative of the type and size of the unit to be installed.

2.3.4 Safe Shutdown Generator

The safe shutdown generator will fire only ULS fuel oil. The generator will be subject to occasional testing to assure operability and used for service only when the transmission connection is lost and the plant shutdowns. When the transmission lines are lost (plant goes black), the generator would start to provide power to maintain the plant in a safe shutdown condition. It will only be run for short test periods when the plant is running, and will otherwise operate only when the plant in down and offsite power is lost.

^{**}Includes the effects of SO₂ oxidation and SCR formation of ammonium sulfates.

As with the diesel engine fire pump, it is estimated that the safe shutdown generator will operate approximately 200 hours per year.

2.3.5 Fuel Oil Storage Tank

The fuel oil storage tank will have a capacity of approximately 990,000 gallons. Volatile Organic Compound (VOC) emissions from the fuel oil storage tank were estimated using the EPA TANKS 4.0 program. Results of the TANKS emission program are included in Appendix C. The VOC emissions from the fuel oil storage tank are approximately 0.16 tons per year (tpy). In accordance with Rule 62-210.300(3)(b)1., F.A.C., the fuel oil storage tank is exempt from the requirement to obtain an air construction permit. However, the fuel oil storage tank VOC emissions were included in the Project potential to emit estimates and information on the tank is included in the application forms.

2.3.6 Mechanical Draft Cooling Tower

The cooling tower water is expected to be wastewater treatment plant reclaimed water that has received high level treatment ("high level" disinfectant). Dissolved solids found in cooling tower drift typically consist of naturally occurring mineral matter, chemicals for corrosion inhibition, etc. Particulate matter is emitted when the drift droplets dispersed in the atmosphere evaporate and leave airborne fine particulate matter formed by crystallizations of dissolved solids.

Based on the type and efficiency of drift eliminators, drift droplets of varying sizes containing dissolved solids can be generated. Studies published by the Cooling Tower Institute have also pointed out that large drift droplets, if emitted, settle out of the tower exhaust air stream and deposit on the ground near the tower. This portion of the drift does not result in particulate matter emissions. Smaller drift droplets may be dispersed in the air and consequently, may evaporate before being deposited in the area surrounding the tower, resulting in emissions of particulate matter. For the purpose of this project, it is assumed that 100 percent of the drift droplets are small enough such that all the drift generated will be dispersed and lose water due to evaporation, resulting in emissions of particulate matter. PM emissions at a circulating water TDS loading of 5,331 ppm were determined to be 6.49 tons per year.

The United States Environmental Protection Agency AP-42 document (Section 13.4) provides a low quality emission factor for estimating PM_{10} emissions from cooling towers. Basically, the AP-42 document assumes that all PM emitted is PM_{10} . FMPA is proposing to use the approach outlined by Reisman and Frisbie to calculate a more realistic PM_{10} emission rate. The paper by Reisman and Frisbie can be found in

Appendix D for reference. This paper points out that at high concentrations of TDS in the circulating water, particulates formed by the mineral matter left after evaporation of moisture from the water droplets will have a higher fraction of particulate greater than 10 microns in diameter than at lower concentrations of TDS. In other words, not all PM emissions are PM₁₀. As TDS increases, total PM emissions increase by virtue of higher TDS. However, the mass fraction of PM₁₀ relative to total PM will decrease because at higher TDS levels, a greater amount of solid particles are larger than 10 microns in diameter.

Based on the design parameters listed in Table 2-1, the PM₁₀ emission estimate procedure outlined in the above referenced document, and Electric Power Research Institute (EPRI) cooling tower test facility data on droplet size distribution (also referenced in the Resiman and Gordon paper), it was determined that at a design recirculating water TDS of 5,331 ppm 27.68 percent of PM mass emissions from the proposed cooling tower are equal to or smaller than PM₁₀. This would result in a total PM₁₀ emissions rate of 1.80 tpy. As a conservative estimate of PM₁₀ emissions the TDS value which results in the highest PM₁₀ emissions was used to estimate the potential emissions from the cooling tower. The maximum PM₁₀ emissions rate was found to correspond with a TDS value of 3,918 ppm. Based on a circulating water TDS loading of 3,918 ppm and the calculated 39.14 percent of PM is PM₁₀, maximum PM₁₀ emissions were determined to be 1.87 tpy. These calculations are presented in Appendix A. Please note that the EPRI drift spectrum was based on a drift eliminator that achieved a tested drift rate of 0.0003 percent. Since the proposed cooling tower has a proposed 0.0005 percent drift rate, it is reasonable to expect that the 0.0003 percent drift rate will produce smaller droplets. Therefore, the EPRI droplet size distribution data can be assumed to be conservative for predicting the fraction of PM₁₀ in the total PM emissions from the proposed cooling tower.

2.4 Maximum Project Potential to Emit

The potential to emit (PTE) for Unit 1 was estimated based on the maximum hourly emission rate for each pollutant at an ambient temperature of 73° F (average annual temperature), considering operation from 40 to 100 percent load, unlimited operation on natural gas and up to 500 hours per year of operation on ULS fuel oil. The PTE for Unit 1 includes the use of the Best Available Control Technology (BACT). BACT for the emissions of NO_x is the use of low-NO_x burners and a SCR system while firing natural gas and the use of water injection and an SCR system when firing fuel oil. The use of natural gas and ULS fuel oil (0.0015 percent sulfur) is considered BACT control for PM/PM₁₀, SO₂, and sulfuric acid mist. Good combustion control is BACT for

CO emissions. The Unit 1 PTE for each pollutant is based on the worst case operating scenario for that pollutant. Therefore, the operating scenario used to calculate the PTE for one pollutant is not necessarily the same operating scenario used to determine the PTE for other pollutants.

The PTE for the auxiliary boiler, the diesel engine fire pump, the safe shutdown generator, the cooling tower and the fuel oil storage tank are also included in the Project's PTE. The auxiliary boiler, diesel engine fire pump, and safe shutdown generator PTE are based on vendor data for the approximate size and type of units that will be installed as part of the Project. The auxiliary boiler PTE is based on unlimited operation. Based on National Fire Protection Association (NFPA) guidelines it is conservatively estimated that the diesel engine fire pump will operate approximately 200 hours per year, and this level of operation was used to determine it's PTE. Similarly, it is conservatively estimated that the safe shutdown generator will operate approximately 200 hours per year, and this level of operation was used to determine its PTE. The fuel oil storage tank potential emissions were determined using the EPA TANKS program. The calculation of the cooling tower emissions is discussed in Subsection 2.3.6. The Project's PTE for each pollutant is summarized in Table 2-2. The footnotes in Table 2-2 provide the basis for the PTE values. The applicable PSD significant emission levels for each pollutant are also included in Table 2-2 for reference purposes.. The printout from a spreadsheet used to calculate the potential to emit is included in Appendix A.

2.5 New Source Review Applicability

The federal Clean Air Act (CAA) New Source Review (NSR) provisions are implemented for new major stationary sources and major modifications under two programs: the Prevention of Significant Deterioration (PSD) program outlined in 40 Code of Federal Regulations (CFR) 51 and 52.21, and the Nonattainment NSR program outlined in 40 CFR 51 and 52. The proposed facility is in an attainment or unclassifiable area with respect to all pollutants. As such, the PSD program will apply to the Project, as administered by the state of Florida under 62-212.400, F.A.C., Stationary Sources – Preconstruction Review, Prevention of Significant Deterioration.

	Table 2-2
PSI	D Applicability

	Project PTE ^(a)	PSD Significant Emission Rate	PSD Review
Pollutant	(tpy)	(tpy)	Required
NO _x	90.0 ^(b)	40	Yes
SO ₂	56.6 ^(c)	40	Yes
со	231.0 ^(b)	100	Yes
PM	176.1 ^(b,d,e)	25	Yes
PM ₁₀	171.4 ^(b,d,e)	15	Yes
VOC	23.4 ^(b,f)	40	No
Sulfuric Acid Mist	22.4 ^(c,g)	7	Yes
Total Reduced Sulfur	negl.	10	No
Hydrogen Sulfide	negl.	10	No
Vinyl Chloride	negl.	1	No
Total Fluorides	negl.	3	No
Mercury	0.001 ^(b,h)	0.1	No
Lead	0.007 ^(b,h)	0.6	No

⁽a) Regardless of operating mode, emissions are based on operation of the combustion turbine at 100 percent load and at an average ambient temperature of 73° F and includes emissions from the duct burner. Includes emissions from the auxiliary boiler, the diesel engine fire pump, and the safe shutdown generator.

Note: PTE calculations are provided in a spreadsheet included in Appendix A.

⁽b) Based on firing ULS fuel oil for 500 hours per year in the combustion turbine and firing natural gas for the remainder of the year.

⁽c) Based on firing natural gas in the combustion turbine for the entire year. Based on a natural gas sulfur content of 2 grains/100 scf.

⁽d)Includes the effects of SO₂ oxidation and formation of ammonium sulfates.

⁽e) Includes front and back half PM/PM₁₀ emissions from the CCTG. Includes emissions from the cooling tower.

⁽f) VOC PTE is based on potential emissions from the Project's combustion source and emissions from the fuel oil storage tank

⁽g)Includes the effects of SO₂ oxidation and assumes 100 percent conversion of SO₃ to sulfuric acid mist (H₂SO₄).

⁽h)Based on AP-42 emission factors.

2.5.1 Prevention of Significant Deterioration

The PSD regulations are designed to ensure that the air quality in existing attainment areas does not significantly deteriorate or exceed the ambient air quality standards (AAQS), while providing a margin for future industrial and commercial growth. PSD regulations apply to major stationary sources and major modifications at existing major sources undergoing construction in areas designated as attainment or unclassifiable.

A major stationary source is defined as any one of the listed major source categories which emits, or has the potential to emit, 100 tpy or more of any regulated pollutant, or 250 tpy or more of any regulated pollutant if the facility is not one of the listed major source categories. The proposed Treasure Coast Energy Center is one of the 28 listed major source categories, and it therefore has a 100 tpy PSD major source threshold. Because the potential to emit of the Project is greater than 100 tpy for at least one PSD pollutant, PSD review is required for all pollutants for which the potential to emit is greater than the PSD significant emissions levels. The estimated potential emissions of NO_x, SO₂, CO, PM/PM₁₀, and sulfuric acid mist (SAM) resulting from the proposed Project exceed the PSD significant emissions levels of 40, 40, 100, 25/15, and 7 tpy, respectively. Therefore, the Project's emissions of NO_x, SO₂, CO, PM/ PM₁₀, and SAM are subject to PSD review. Because emissions of VOC are below the PSD significant emissions level of 40 tpy, the Project is not subject to PSD review for VOCs. The PSD review includes a BACT analysis, air quality impact analysis (AQIA), and an assessment of the Project's total impact on general residential and commercial growth, soils and vegetation, and visibility, as well as a Class I impact analysis. These analyses are included in Sections 3.0, 4.0, and 5.0.

2.6 Regulatory Review

This section provides a review of rule applicability for the various emission units that are a part of the Project.

2.6.1 Rule Applicability to Unit 1

The following Sections include a discussion of the applicability of regulations to the Unit 1 combustion turbine and/or the duct burner.

2.6.1.1 CT MACT. On March 5, 2004, the United States Environmental Protection Agency (EPA) published final national emission standards for hazardous air pollutants (NESHAP) for stationary combustion turbines. This rule, found at 40 CFR Part 63 Subpart YYYY, is commonly referred to as the CT MACT. The CT MACT is applicable to stationary gas turbines located at major sources of hazardous air pollutants (HAPs). A

major source of HAPs is a site that emits or has the potential to emit any single HAP at a rate of 10 tons or more per year or any combination of HAP at a rate of 25 tons or more per year. Potential HAP emissions at the facility were estimated using USEPA AP-42 emission factors. The following emission units were included in the HAP emissions analysis:

- The combustion turbine.
- The HRSG duct burner.
- The auxiliary boiler.
- The diesel engine fire pump.
- The safe shutdown generator.

The potential to emit for any combination of HAP at the Treasure Coast Energy Center is 12.5 tons per year. The maximum potential to emit of any single individual HAP is 5.5 tons per year of formaldehyde. It should be noted that these emission calculations are based on AP-42 emission factors, which are believed to provide a very conservative estimate of HAP emissions from the type of combustion turbine to be installed at the Treasure Coast Energy Center. Using this conservative basis, the potential to emit level is well below the HAP major source levels, and as such, the site is not a major source of HAPs. Because the site is not a major source of HAPs, the CT MACT standard does not apply to Unit 1. Spreadsheets showing the HAP emission calculations for the Project are included in Appendix A.

2.6.1.2 New Source Performance Standards (NSPS). The combustion turbine is subject to the Standards of Performance for Stationary Gas Turbines, as revised July 8, 2004. This type of standard is commonly referred to as a New Source Performance Standard (NSPS). This NSPS is found at 40 CFR 60 Subpart GG and is adopted by reference in Rule 62-204.800(8)(b)39, F.A.C.

The duct burner is subject to the Standards of Performance for Electric Utility Steam Generating Units for Which Construction is Commenced After September 18, 1978. This NSPS is found at 40 CFR 60 Subpart Da and is adopted by reference in Rule 62-204.800(8)(b)2, F.A.C.

As a proposed new NSPS standard, published in the Federal Register on February 18, 2004, the Standards of Performance for Stationary Combustion Turbines for Which Construction is Commenced After February 18, 2005 or for Which Modification or Reconstruction is Commenced on or After [Date 6 Months After Date Final Rule is Published in the Federal Register] will be applicable to Unit 1, when/if it becomes final, if it becomes final as proposed. This NSPS will be found at 40 CFR 60 Subpart KKKK when/if it is made final.

When/if the proposed NSPS Subpart KKKK becomes final, if it becomes final as proposed, the Unit 1 combustion turbine will not be subject to NSPS Subpart GG. As stated in 40 CFR 60.4305(b) of proposed Subpart KKKK, stationary combustion turbines regulated under 40 CFR 60 Subpart KKKK are exempt from the requirements of 40 CFR 60 Subpart GG.

Proposed revisions to NSPS Subpart Da, Standards of performance for Electric Utility Steam Generating Units for Which Construction is Commenced After September 18, 1978, were published in the Federal Register on February 28, 2005. Under 60.40a(b) of the proposed Subpart Da revisions and under 40 CFR 60.4305(b) of proposed Subpart KKKK, heat recovery steam generators and duct burners regulated under Subpart KKKK are exempted from the requirements of 40 CFR 60 Subpart Da. Therefore, when/if finalized, under proposed NSPS Subpart KKKK and proposed revisions to NSPS Subpart Da, the Unit 1 duct burner will not be subject to NSPS Subpart Da.

2.6.2 Rule Applicability to the Natural Gas Auxiliary Boiler

The Standards of Performance for Small Industrial-Commercial-Institutional Steam Generating Units, NSPS Subpart Dc, applies to each steam generating unit that has a maximum design capacity of 100 mmBtu/h or less, but greater than 10 mmBtu/h. Because the Project natural gas auxiliary boiler has a maximum heat input rate of less than 10 mmBtu/h, it is not subject to 40 CFR Subpart Dc.

The natural gas auxiliary boiler is subject to Rule 62-296.406, F.A.C., Fossil Fuel Steam Generators with Less Than 250 Million Btu Per Hour Heat Input, New and Existing Emission Units. By this rule the auxiliary boiler is subject to a 20 percent opacity standard and is required to implement BACT for PM and SO₂. As discussed in Section 3, the use of natural gas and good combustion practices is considered BACT for this emissions unit.

2.6.3 Rule Applicability for the Diesel Engine Fire Pump

There are no NSPS regulations applicable to this emissions unit. The *National Emission Standards for Reciprocating Internal Combustion Engines* MACT standard is only applicable to emission units at a facility that is a major source of HAPs. This MACT standard is found at 40 CFR 63 Subpart ZZZZ. As discussed in Section 2.6.1.1, the Energy Center will not be a major source of HAPs, and as such 40 CFR 63 Subpart ZZZZ does not apply to this emissions unit. None of the standards included in 62-296, F.A.C. apply to the diesel engine fire pump.

Because the diesel engine fire pump falls under the categorical emission unit exemption given at Rule 62-210.300(3)(a)22, F.A.C. for fire and safety equipment, the

diesel engine fire pump is exempt from the preconstruction review permitting requirements of Chapter 62-212, F.A.C. The diesel engine fire pump is included in the list of exempt emission units given in Attachment G of the application forms. While the diesel engine fire pump is considered exempt from permitting requirements, the projected potential emissions are included in the Project potential to emit calculations and its' emissions were included in the ambient air quality impact analysis (AAQIA). A set of emissions unit information forms for this emissions unit is also included with the application forms.

2.6.4 Rule Applicability for the Safe Shutdown Generator

There are no NSPS regulations applicable to this emissions unit. The *National Emission Standards for Reciprocating Internal Combustion Engines* MACT standard is only applicable to emission units at a facility that is a major source of HAPs. This MACT standard is found at 40 CFR 63 Subpart ZZZZ. As discussed in Subsection 2.6.1.1, the new Energy Center will not be a major source of HAPs, and as such 40 CFR 63 Subpart ZZZZ does not apply to this emissions unit. None of the standards included in 62-296, F.A.C. apply to the safe shutdown generator.

2.6.5 Rule Applicability to the 990,000 Gallon Fuel Oil Storage Tank

The fuel oil storage tank to be added as part of the Project is estimated to have a capacity of slightly less than 990,000 gallons. The Standards of Performance for volatile organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984, as revised October 15, 2003, does not apply to storage vessels which store a liquid with a vapor pressure less than 3.5 kPa. This NSPS is found at 40 CFR 60 Subpart Kb and is adopted by reference in Rule 62-204.800(8)(b)16, F.A.C. Because the vapor pressure of ULS fuel oil is less than 3.5 kPa, this storage tank is not subject to 40 CFR 60 Subpart Kb. None of the standards included in 62-296, F.A.C. apply to the fuel oil storage tank.

Because the fuel oil storage tank meets the criteria of 62-210.300(3)(b)1, the fuel oil storage tank is considered exempt from the preconstruction review permitting requirements of Chapter 62-212, F.A.C. The fuel oil storage tank is included in the list of exempt emission units given in Attachment G of the application forms. However, potential emissions from this emissions unit are included in the Project PTE calculations to ensure that the emissions from this emissions unit would not cause the Project PTE to exceed the PSD significant emissions level for VOCs. A set of emissions unit information forms for this emissions unit is also included with the application forms.

2.6.6 Rule Applicability for the Mechanical Draft Cooling Tower

There are no MACT standards or NSPS standards that apply to the cooling tower. None of the standards included in 62-296, F.A.C. apply to the cooling tower.

2.6.7 Excess Emissions

As with other combined cycle combustion turbines of this size and type, excess emissions during startup, shutdown and malfunction are likely to exceed the duration of excess emissions allowed per Rule 62-210.700(1), F.A.C. In accordance with Rule 62-210.700(5), F.A.C., FMPA is requesting that the air permit for the Project allow for excess emissions from startups and shutdowns greater than 2 hours per 24 hour period. FMPA requests that a condition similar to condition 15 of the APPLICABLE STANDARDS AND REGULATIONS Section of the Florida Power & Light Turkey Point Unit 5 permit issued by FDEP on February 8, 2005 be included in the Project permit. In general, it is requested that in a 24 hour period, this condition allow for six hours of excess emissions during a cold start of the steam turbine/HRSG system, four hours of excess emissions during a warm start of the steam turbine/HRSG, three hours of excess emissions for the shutdown of the combined cycle operation and one hour of excess emissions for a fuel switch. It is also requested that in the event there is a trip during a startup or during a 24-hour period that contains a startup, the permit allows for additional excess emissions during a startup subsequent to a unit trip (i.e. the allowable excess emissions clock starts over after a unit trip which results in the need to restart the unit).

2.6.8 DLN Tuning

As allowed in the Florida Power & Light Turkey Point Unit 5 permit issued by FDEP on February 8, 2005, FMPA is requesting that the permit for this project allow for exclusion of CEMS data collected during initial or other major DLN tuning sessions from the CEMS compliance demonstration. FMPA is requesting that a condition similar to condition 16 of the APPLICABLE STANDARDS AND REGULATIONS Section of the Florida Power & Light Turkey Point Unit 5 permit issued by FDEP on February 8, 2005 be included in the Project permit. The following is example permit language:

"DLN Tuning: Excess emissions of NOx, CO, and opacity is allowed during DLN tuning sessions. CEMS data collected during initial or other major DLN tuning sessions shall be excluded from the CEMS compliance demonstration provided the tuning session is performed in accordance with the manufacturer's specifications. A "major tuning session" would occur after completion of initial construction, a combustor change-out, a major repair or maintenance to a

combustor, or other similar circumstances. Prior to performing any major tuning session, the permittee shall provide the Compliance Authority with an advance notice that details the activity and proposed tuning schedule. The notice may be by telephone, facsimile transmittal, or electronic mail. [Design; Rule 62-4.070(3), F.A.C.]"

3.0 Best Available Control Technology

A best available control technology (BACT) analysis for the Project has been included as Appendix E. Emissions for the BACT analysis are based on unlimited natural gas firing for Unit 1 and an average ambient temperature of 78° F. The following is a summary of the BACT determination for Unit 1.

- Nitrogen oxides (NO_x) emissions--BACT was determined to be the use of low-NO_x burners and an SCR to achieve 2 ppmvd at 15 percent O₂ when firing natural gas and the use of water injection and an SCR to achieve 8 ppmvd at 15 percent O₂ when firing ULS fuel oil.
- Carbon monoxide (CO) emissions--BACT was determined to be the use of good combustion practices when firing either natural gas or ULS fuel oil.
- Particulate (PM/PM₁₀) emissions--BACT was determined to be the use of good combustion controls and the use of natural gas and ULS fuel oil with less than 0.0015 percent sulfur by weight.
- Volatile Organic Compounds (VOC) emissions--A BACT analysis was not required for this emission parameter since annual emissions will be below the PSD major modification thresholds.
- Sulfur dioxide (SO₂) emissions--BACT was determined to be the use of natural gas and ULS fuel oil with less than 0.0015 percent sulfur.
- Sulfur acid mist (H₂SO₄) emissions--BACT was determined to be the use of natural gas and ULS fuel oil with less than 0.0015 percent sulfur.

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4.0 Air Quality Impact Analysis

The following sections discuss the air dispersion modeling performed for the PSD air quality impact analysis for those PSD pollutants which will have a PTE greater than the PSD significant emission rate (i.e. CO, NO_x, PM/PM₁₀, and SO₂). The air dispersion modeling analysis was conducted in accordance with EPA's air dispersion modeling guidelines (incorporated as Appendix W of 40 CFR 51), as well as a mutually agreed upon air dispersion modeling protocol submitted to FDEP on behalf of FMPA in a letter from Black & Veatch dated January 7, 2005. The FDEP provided approval of the protocol via email on January 13, 2005. Comments on the protocol were provided by EPA Region 4 via FDEP on February 7, 2005. Responses to the EPA comments were provided to FDEP on February 18, 2005. On February 22, 2005 FDEP responded that the EPA indicated that all of the responses to their comments were appropriate. The National Park Service (NPS) provided comments on the Class I protocol on February 28, 2005. A response to the NPS comments was provided to FDEP on March 3, 2005. A copy of the protocol, correspondence indicating FDEP and EPA approval of the protocol, and correspondence regarding the NPS comments are presented in Appendix F.

4.1 Model Selection

The Industrial Source Complex Short-Term (ISCST3 Version 02035) air dispersion model was used to predict maximum ground level concentrations associated with the Project emissions. The ISCST3 model is an EPA approved, steady-state, straight-line Gaussian plume model, which may be used to assess pollutant concentrations from a wide variety of sources associated with an industrial source complex.

4.2 Model Input and Options

This section discusses the model input parameters, source and emission parameters, and the ISCST3 model default options and input databases.

4.2.1 Model Input Source Parameters

The ISCST3 model was used to determine the maximum predicted ground-level concentration for each pollutant and applicable averaging period resulting from various operating loads, fuels, and ambient temperatures. Performance data for the combustion turbine operating with separate fuels (natural gas and ultra low sulfur fuel oil) at several different loads (40, 50, 75, and 100 percent) over a range of ambient temperatures (26, 59, 73, and 100° F) are included in Appendix B. The corresponding stack parameters and emission rates for each load and ambient temperature considered in the analysis are

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presented in Table 4-1. For the 100 percent load cases, the parameters in Table 4-1 are "enveloped" over the different operating scenarios as provided in Appendix B. "Enveloping" is the process in which a representative set of stack parameters and pollutant emission rates are utilized to produce the worst-case plume dispersion conditions and highest model predicted concentrations (i.e., lowest exhaust temperature and exit velocity and the highest emission rate).

Emissions from the auxiliary boiler, diesel engine fire pump, safe shutdown generator, and the cooling tower were also included in the modeling. Emissions data for these emission units are included in Appendix A. Because the diesel engine fire pump and the safe shutdown generator are only operated in emergency situations and for occasional testing to ensure operability, emissions from these units in the modeling are based on operating 1 hour per day and 200 hours per year.

4.2.2 Land Use Dispersion Coefficient Determination

The EPA's land use method was used to determine whether rural or urban dispersion coefficients should be used in the ISCST3 air dispersion model. In this procedure, land circumscribed within a 3 km radius of the site was classified as rural or urban using the Auer land use classification method. Based on a visual inspection of the USGS 7.5 minute topographic map of the proposed Project's location, it was concluded that over 50 percent of the area surrounding the Project is classified as rural. Accordingly, the rural dispersion modeling option was used in the ISCST3 air dispersion modeling.

4.2.3 GEP Stack Height Determination

The Project's proposed buildings and structures were analyzed to determine their potential to influence the dispersion of stack emissions. Building and structure dimensions, as well as relative locations, were entered into EPA's Building Profile Input Program (BPIP) to produce an ISCST3 input file with the proper Huber-Snyder or Schulman-Scire direction specific building downwash parameters. The BPIP formula GEP height for the combined cycle Unit 1 stack is 64.01 m (210 ft). The proposed Project stack height is 51.81 m (170 ft). As such, direction-specific downwash parameters from the BPIP program were included in the ISCST3 air dispersion modeling analysis.

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Table 4-1
Stack Parameters and Pollutant Emissions
Used in ISCST3 Modeling Analysis

	Load	Ambient Temperature	Stack Height	Stack Diameter	Exit Velocity	Exit Temp	Pollutant Emission Rate (lb/h)				
Fuel ^(a)		(°F)	(ft)	(ft)	(ft/s)	(°F)	NO _x	SO ₂	PM/PM ₁₀ (b)	СО	
	100	100	170	18	58	166	16.10	12.55	38.00	49.20	
		73	170	18	63	168	16.50	12.89	38.00	50.10	
		59	170	18	64	166	16.90	13.20	38.00	51.40	
		26	170	18	68	167	17.50	13.64	38.00	52.30	
	75	100	170	18	48	173	9.60	7.45	22.60	22.00	
		73	170	18	51	172	10.20	7.97	23.00	23.00	
		59	170	18	51	169	10.40	8.18	23.10	24.00	
NG		26	170	18	53	167	11.10	8.60	23.40	25.00	
NG	50	100	170	18	40	167	7.60	5.93	21.70	18.40	
		73	170	18	42	164	8.00	6.36	22.00	19.10	
		59	170	18	42	161	8.30	6.54	22.10	20.00	
		26	170	18	43	158	8.70	6.89	22.30	20.30	
	40	100	170	18	37	165	6.70	5.26	19.00	52.30	
		73	170	18	38	162	7.10	5.61	19.00	52.30	
		59	170	18	38	158	7.30	5.76	19.00	18.00	
		26	170	18	39	155	7.80	6.08	19.00	18.40	

Table 4-1 (Continued) Stack Parameters and Pollutant Emissions Used in ISCST3 Modeling Analysis

		Ambient Temperature	Stack Height	Stack Diameter	Exit Velocity	Exit Temp	Pollutant Emission Rate (lb/h)				
Fuel ^(a)	Load	(°F)	(ft)	(ft)	(ft/s)	(°F)	NO _x	SO ₂	PM/PM ₁₀ ^(b)	СО	
	100	100	170	18	68	249	73.20	5.91	51.20	82.30	
		73	170	18	74	251	76.00	6.04	49.90	86.20	
		59	170	18	76	251	78.00	6.17	52.00	88.70	
		26	170	18	81	252	81.10	6.29	50.00	92.40	
	75	100	170	18	56	250	45.00	2.19	35.40	49.00	
FO		73	170	18	58	248	48.00	2.34	35.50	51.00	
10		59	170	18	60	245	49.80	2.42	36.20	52.50	
		26	170	18	62	247	52.00	2.52	35.60	54.20	
	50	100	170	18	46	243	35.10	1.72	35.10	41.10	
		73	170	18	48	243	37.60	1.84	35.10	43.00	
		59	170	18	49	243	39.30	1.91	35.70	43.50	
		26	170	18	50	243	40.70	1.99	35.20	45.00	

⁽a) NG – Natural Gas, FO – Ultra Low Sulfur Fuel Oil.
(b) PM/PM₁₀ represents both front and back half emissions. PM/PM₁₀ emissions for natural gas firing 40 percent load case are based on results of air dispersion modeling and engineering judgment.

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4.2.4 Model Defaults

The following standard USEPA default regulatory modeling options were initialized in the ISCST3 air dispersion modeling:

- Final plume rise.
- Stack-tip downwash.
- Buoyancy induced dispersion.
- Default vertical wind profile exponents and vertical potential temperature gradient values.
- Calm processing option.
- Flat terrain option.

4.2.5 Receptor Grid and Terrain Considerations

The air dispersion modeling receptor locations were established at appropriate distances to ensure sufficient density and aerial extent to adequately characterize the pattern of pollutant impacts in the area. Specifically, a nested rectangular grid network that extends 10 km from the center of the proposed Project was used. The rectangular grid network consists of 100 m spacing from the proposed fenceline out to 1 km, 250 m spacing from 1 to 2.5 km, 500 m spacing from 2.5 to 5 km, and then 1,000 m spacing from 5 to 10 km. Receptor spacing of 100 m intervals was used along the Project's fenceline, and a 100 m fine grid was used at the maximum impact receptors. The flat terrain option was used for all receptor points. Figure 4-1 illustrates the nested rectangular grid, fence line receptors, and the relative location of the emission source and downwash structures.

4.2.6 Meteorological Data

The ISCST3 air dispersion model requires hourly input of specific surface and upper-air meteorological data. These data include the wind flow vector, wind speed, ambient temperature, stability category, and the mixing height. Five years (1987-1991) of surface and upper air meteorological data from West Palm Beach were used in the ISCST3 air dispersion modeling analysis. These meteorological data were downloaded from EPA's SCRAM web site and processed with PCRAMMET to combine the surface and mixing height data, interpolate hourly mixing heights from the twice-daily mixing heights, and calculate atmospheric stability class.

4.3 Model Results

As presented in Section 2.0, the Project's PTE exceeds the PSD significant emission thresholds for NO_x, SO₂, PM/PM₁₀, and CO. In accordance with the approved modeling protocol, ISCST3 air dispersion modeling was performed (as described in the preceding

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sections) using the emission rates for NO_x, SO₂, PM/PM₁₀, and CO for each applicable averaging period. Table 4-2 compares the maximum model predicted concentrations for each pollutant and applicable averaging period with the PSD Class II significant impact levels (SILs) and the pre-construction monitoring requirements. As Table 4-2 indicates, the Project's maximum model-predicted concentrations are less than the PSD Class II SILs for each pollutant and applicable averaging period. Therefore, under the PSD program, no further air quality impact analyse (i.e., PSD increment and Ambient Air Quality Standards analyses) are required. As the Projects' major source of emissions is the combustion turbine; for informational purposes, the maximum impacts from the combustion turbine without the contribution of the ancillary equipment are presented in Table 4-3.

If any of the maximum impact source groups from each pollutant and averaging period, or the controlling impacts (i.e., a concentration within 10 percent of the maximum impact) from such a source group, occurred at the edge of or beyond the 100 m fine grid, a 100 m refined receptor grid would be placed around the impact to ensure that an absolute maximum concentration was obtained from the model. This procedure was not required for any pollutants, as all of the maximum impacts and controlling impacts were within the 100 m fine grid.

Additionally, the maximum predicted concentrations are less than the preconstruction monitoring de minimis levels for each pollutant and applicable averaging period. Therefore, by this application, the applicant requests an exemption from the PSD pre-construction monitoring requirements.

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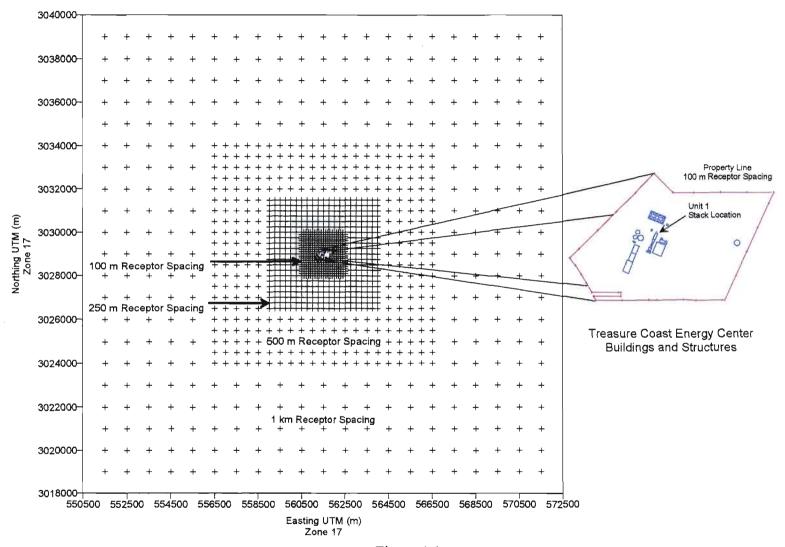


Figure 4-1
Receptor Location Plot

Table 4-2
ISCST3 Model-Predicted Class II Impacts

				Model-Pre	edicted Imp	oact ^(a) (μg/m	PSD · Class II		De Minimis			
	Averaging		Natural Gas				Fuel Oil			Exceed	Monitoring Level ^(c)	Pre-Construction Monitoring
Pollutant	Period	100%	75%	50%	40%	100%	75%	50%	SIL ^(b) (μg/m³)	SIL?	(μg/m ³)	Required?
NO _x	Annual	0.61	0.62	0.64	0.65	0.61	0.63	0.66	1	NO	14	NO
	Annual	0.05	0.06	0.07	0.08	0.05	0.05	0.05	1	NO		NO
SO ₂	24 Hour	1.21	1.15	1.35	1.39	0.37	0.37	0.37	5	NO	13	NO
	3 Hour	2.89	2.25	2.44	2.43	1.36	1.36	1.36	25	NO		NO
PM/PM ₁₀ ^(d)	Annual	0.20	0.22	0.27	0.30	0.20	0.20	0.23	1	NO		NO
PIVI/PIVI ₁₀	24 Hour	4.02	3.90	4.86	4.79	2.75	3.32	4.69	5	NO	10	NO
	8 Hour	10.45	10.34	10.34	18.51	10.34	10.34	10.34	500	NO	575	NO
СО	1 Hour	102.14	102.14	102.14	102.14	102.15	102.14	102.14	2,000	NO		NO

⁽a) Impacts represent the highest first high model-predicted concentration from all 5 years of meteorological data modeled at each corresponding load.

⁽b) Predicted impacts that are below the specified level indicate that the proposed project will not have predicted significant impacts for that pollutant and further modeling is not necessary for that pollutant.

⁽c) This criteria is used to determine if pre-construction ambient air monitoring is required to assess current and future compliance with Ambient Air Quality Standards.

⁽d) Note that the PM₁₀ impacts are below the PSD Class II SILs and the NAAQS for PM_{2.5} are significantly greater than the PM₁₀ SILs. Therefore, if one were to conservatively assume that PM_{2.5} impacts would be the same as the PM₁₀ impacts, then the impacts would be significantly below the PM_{2.5} NAAQS.

Table 4-3
ISCST3 Model-Predicted Combustion Turbine Impacts

	Model-Predicted Impact ^(a) (μg/m ³) PSD											
			N		PSD							
	Averaging		Natur	al Gas			Fuel Oil	Class II SIL ^(b)	Exceed			
Pollutant	Period	100%	75%	50%	40%	100%	75%	50%	$(\mu g/m^3)$	SIL?		
NO _x	Annual	0.040	0.030	0.051	0.066	0.090	0.071	0.093	1	NO		
	Annual	0.031	0.023	0.040	0.052	0.007	0.003	0.005	1	NO		
SO ₂	24 Hour	1.106	1.080	1.264	1.297	0.180	0.164	0.197	5	NO		
	3 Hour	2.818	2.184	2.372	2.359	0.640	0.379	0.410	25	NO		
DM/DM	Annual	0.095	0.066	0.142	0.168	0.063	0.053	0.093	1	NO		
PM/PM ₁₀	24 Hour	3.347	3.221	4.182	4.117	1.563	2.641	4.016	5	NO		
	8 Hour	8.519	4.971	5.634	16.58	4.338	6.112	7.185	500	NO		
СО	1 Hour	16.38	9.219	9.629	27.53	16.42	12.93	13.99	2,000	NO		

^(a)Impacts represent the highest first high model-predicted concentration from all five years of meteorological data modeled at each corresponding load.

⁽b) Predicted impacts that are below the specified level indicate that the proposed project will not have predicted significant impacts for that pollutant and further modeling is not necessary for that pollutant.

⁽c) This criteria is used to determine if pre-construction ambient air monitoring is required to assess current and future compliance with Ambient Air Quality Standards.

5.0 Additional Impact Analyses

The following sections discuss the proposed Project's impacts upon commercial, residential, and industrial growth, as well as vegetation and soils, and the nearest Federal Class I area.

5.1 Commercial, Residential, and Industrial Growth

The proposed project is to be located at the new Treasure Coast Energy Center near Fort Pierce, St. Lucie County, Florida. Because the proposed project is being installed to meet the existing and current projected electrical demands of the surrounding area, it is anticipated that little growth will be associated with its operation. There will be an increase in the local labor force during the construction phase of the Project, but this increase will be temporary, short-lived, and will not result in permanent/significant commercial and residential growth occurring in the vicinity of the project.

The electrical generating capacity created by the Project will not have a significant effect upon the industrial growth in the immediate area, considering that the electrical generating capacity will be sold to the grid as opposed to a nearby industrial host.

Population increase is a secondary growth indicator of potential increases in air quality levels. Changes in air quality due to population increase are related to the amount of vehicle traffic, commercial/institutional facilities, and home fuel use. According to the US Census Bureau, the population of St. Lucie County has grown by 28.3 percent between the 1990 and 2000 censuses. In line with the population growth, the net number of new, permanent jobs which will be created by the Project is estimated to be little to none. It can be concluded that the air quality impacts associated with secondary growth will not be significant because the increase in population due to the operation of the Project will be very small, compared to the overall existing population size of the surrounding area.

5.2 Vegetation and Soils

Combustion turbine projects are typically considered "clean facilities" that have very low predicted ground level pollutant impacts. The low predicted impacts are the direct result of complete combustion and very effective pollutant dispersion. Dispersion is enhanced by the thermal and momentum buoyancy characteristics of the combustion turbine exhaust. Therefore, the Project's impacts on soils and vegetation will be minimal.

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The AAQS were established to protect public health and welfare from any adverse effects of air pollutants. The definition of public welfare also encompasses vegetation and soils. Specifically, and as indicated in the *Draft New Source Review Workshop Manual* (EPA, 1990), ambient concentrations of NO₂, SO₂, and PM/PM₁₀ below the secondary AAQS will not result in harmful effects for most types of soils and vegetation.

The criteria pollutants which triggered an additional impact analysis include NO_x , SO_2 , and PM/PM_{10} . The modeled impacts were compared to the secondary AAQS as the basis for assessing impacts. It can be inferred from the modeling in Section 4.0 that the NO_x , SO_2 , and PM/PM_{10} impacts are below the AAQS. The impacts are even less than the much lower significant impact level thresholds. Because the Project's emissions do not significantly impact the AAQS, it is reasonable to conclude that no adverse effects on soils and vegetation will occur.

5.3 Class I Area Impact Analysis

As part of the air impact evaluation for the proposed Project, analyses of the Project's effect on both the Everglades National Park (ENP) and the Chassahowitzka Wilderness Area (CWA) were performed. The ENP is a PSD Class I area located in southern Florida, approximately 180 km south-southwest of the Project site. The CWA is a PSD Class I area located in central Florida along the Gulf of Mexico coast, approximately 260 km northwest of the Project site. Federal Class I areas are afforded special environmental protection through the use of Air Quality Related Values (AQRVs). The AQRVs of interest in this analysis are regional haze and deposition. Additionally, Class I Significant Impact Levels (SILs) were evaluated and compared to the recommended thresholds. Figure 5-1 presents the location of the proposed Project site with respect to the ENP and CWA.

The methodology of the California Puff (CALPUFF) analysis followed those procedures recommended in the National Park Service's (NPS) Federal Land Managers' Air Quality Related Values Workgroup (FLAG) Phase I Report dated December 2000, Earth Tech, Inc.'s Guide for Applying the EPA Class I Screening Methodology with the CALPUFF Modeling System dated September 2001, the Long-Range-Transport Screening Technique Using CALPUFF document jointly authored by the NPS and the EPA, and an air dispersion modeling protocol sent to FDEP in response to NPS comments (received February 28, 2005) on Black & Veatch's original protocol and subsequent responses to EPA comments, via email, on March 3, 2005 (Appendix F). The following sections include discussions of the air modeling approach to assess impacts at ENP and CWA as well as the model-predicted impacts from the Project onto the ENP and CWA.

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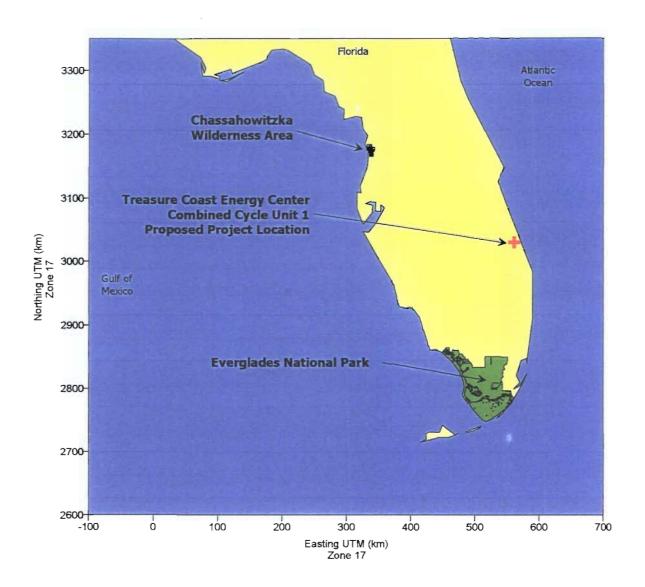


Figure 5-1
Proposed Project Location with Respect to
Everglades National Park & Chassahowitzka Wilderness Area

138859 5-3

5.3.1 Model Selection

The CALPUFF (Version 5.711A, Level 040716) air modeling system was used to model the Project and assess the AQRVs at ENP and CWA. CALPUFF is a non-steady state Lagrangian Gaussian puff long-range transport model that includes algorithms for building downwash effects as well as chemical transformations (important for visibility controlling pollutants), and wet/dry deposition. CALPUFF was used in the "screening mode" of the model commonly referred to as CALPUFF Lite. CALPUFF Lite utilizes a modified meteorological data file for use in the ISCST3 air dispersion model, thus bypassing the need to run CALMET, an involved model designed to generate a three dimensional wind field with USGS terrain and land use data files, while retaining the required conservatism of a screening model.

5.3.2 CALPUFF Model Settings

The CALPUFF settings contained in Table 5-1 were used for the modeling analyses.

5.3.3 Building Wake Effects

The CALPUFF analysis included the proposed facility's building dimensions to account for the effects of building-induced downwash on the emission sources. Dimensions for all significant building structures were processed with the Building Profile Input Program (BPIP), Version 04112, and included in the CALPUFF model input.

5.3.4 Receptor Locations

The CALPUFF ENP analysis used three rings of discrete Cartesian receptors located at a distance equal to that of the nearest, equidistant, and farthest boundary of ENP and the location of the Project. Specifically, the rings consists of receptor spacing of every 1-degree (i.e., 360 receptors per ring) beginning with the closest ring at a 181.1 km distance from the Project, the intermediate ring at a 232.6 km distance from the Project, and the farthest ring at a distance of 284.1 km. The elevation for all of the discrete Cartesian receptors were conservatively assumed to equal the maximum elevation representative of the ENP in the database of discrete receptors created and distributed by the NPS for standardized use in refined Class I analyses. The maximum elevation presented in the array of discrete Cartesian receptors in the NPS database for ENP was 1 meter and was applied to each receptor on all three rings effectively representing ENP in every direction from the Project. Receptor rings serve to introduce conservatism into screening level modeling.

Table 5-1 CALPUFF Model Settings				
Parameter	Setting			
Pollutant Species	SO ₂ , SO ₄ , NO _x , HNO ₃ , NO ₃ , PM ₁₀ , PM _{0.05} , PM _{0.10} , PM _{0.15} , PM _{0.20} , PM _{0.25} , and PM _{1.00}			
Chemical Transformation	MESOPUFF II scheme			
Deposition	Include both dry and wet deposition, plume depletion			
Meteorological/Land Use Input	ISC type data processed for wet deposition			
Plume Rise	Stack-tip downwash			
Dispersion	Puff plume element, PG/MP coefficients, rural mode, ISC building downwash scheme			
Terrain Effects	Partial plume path adjustment			
Output	Create binary concentration and wet/dry deposition files including output species for all pollutants.			
Model Processing	Regional Haze: Highest predicted 24 hour change as processed by CALPOST. Deposition: Highest predicted annual total sulfur and nitrogen values in deposition units. Class I SILs: Highest predicted concentrations at the applicable averaging periods for those pollutants that exceed the respective PSD Significant Emission Levels (SELs).			
Background Values	Monthly Ammonia: 10 ppb; Monthly Ozone: 80 ppb			

Due to the area's small size, the CALPUFF CWA analysis used two rings of discrete Cartesian receptors located at a distance equal to that of the nearest and farthest boundary of CWA and the location of the Project. Specifically, the closest ring consists of receptor spacing of every 1-degree beginning at a 260.5 km distance from the Project, while the farthest ring begins at a distance of 274.7 km with receptor spacing of every 1-degree. The elevation for all of the discrete Cartesian receptors were conservatively assumed to equal the maximum elevation representative of the CWA in the NPS database of discrete receptors of Class I areas. The maximum elevation presented in the array of discrete Cartesian receptors in the NPS database for CWA was 3 meters and was applied to each receptor on the two rings effectively representing CWA in every direction from the Project.

5.3.5 Modeling Domain.

The size of the domain used for the modeling was based on recommendations found in the guidance document *Interagency Workgroup on Air Quality Modeling (IWAQM) Phase II*, dated December 1998. Specifically, the guidance document states that the domain should extend at least 50 km beyond the outer most receptor ring in each of the north, south, east, and west directions to allow for puffs to return to a Class I area due to a recirculating wind pattern.

Since the screening methodology uses meteorological data from a single ISC meteorological data file, there is no spatial variation in meteorological or geophysical properties. Therefore, the minimum grid cell configuration of 2 grid cells in the x-direction and 2 grid cells in the y-direction was used (4 grid cells total). A single layer was used in the vertical since wind speed measurements taken at an emometer height will be scaled to stack-top height, as in ISC. Therefore, the two cell face heights were set to 0 meters (ground-level) and 5,000 meters.

The outer most receptor rings extended 284.1 km and 274.7 km from the Project site for the ENP and CWA, respectively. Since the CWA domain was completely encompassed by the ENP domain, only one domain was utilized in the modeling analysis. The resulting grid cells are 334.1 km on a side, producing a 50-km buffer for ENP and a 59.4-km buffer for CWA. The modeling analysis was performed in the UTM coordinate system. The southwest corner of the domain is the origin and is located at 227.416 km Easting and 2,694.896 km Northing (based on UTM Zone 17, North American Datum (NAD) 1927 coordinates). Figures 5-2 and 5-3 illustrate the size and location of the modeling domain and associated receptors with respect to ENP and CWA, respectively.

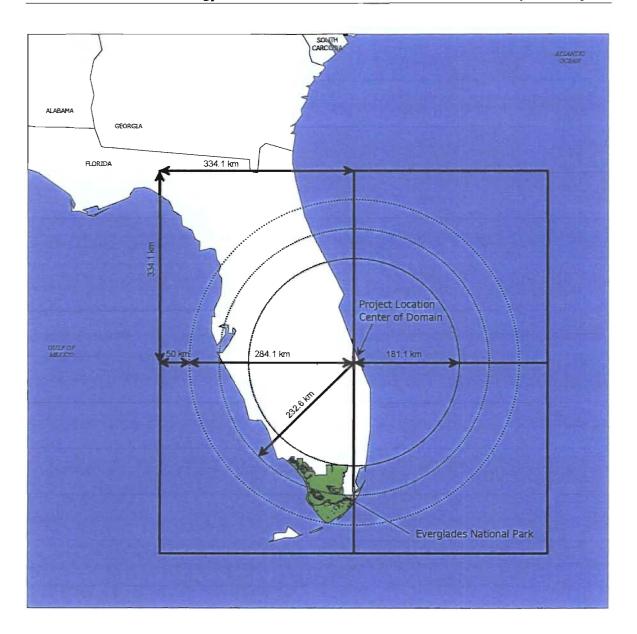


Figure 5-2 Modeling Domain

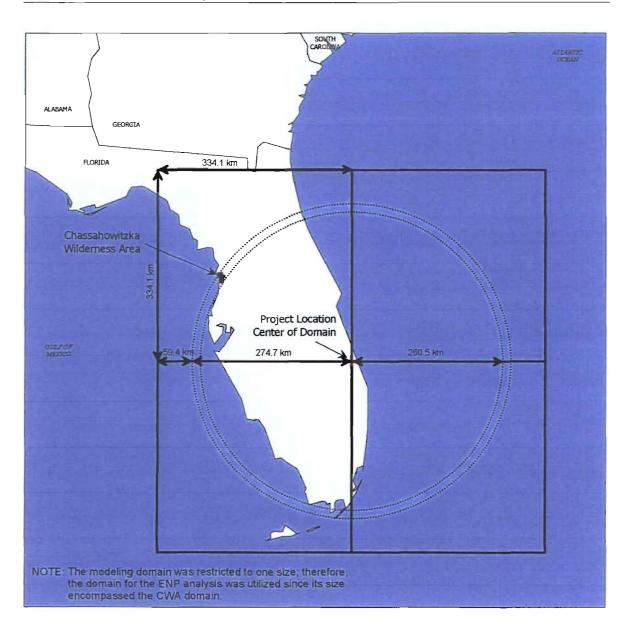


Figure 5-3 Modeling Domain

5.3.6 Meteorological Data

The meteorological data that was used in the CALPUFF Lite model consisted of five years (1987-1991) of National Weather Service data. The data set included surface observations and upper air, twice-daily mixing height data for West Palm Beach, Florida, downloaded from the EPA's SCRAM website. The data were processed with CPRammet to give CALPUFF enough information to perform the Mesopuff II chemistry transformations. CPRammet is a modified version of the EPA meteorological processor PCRammet. It was created by Earth Tech, the developers of the CALPUFF modeling system. CPRammet was designed to alleviate two incompatibilities between PCRammet and the CALPUFF model: 1) PCRammet will not produce the necessary extended ISCST3 variables (e.g., friction velocity, Monin-Obukhov length, relative humidity, solar radiation, etc.) when input data are in CD-144 format and 2) PCRammet will not report solar radiation when an observed value is missing.

The data were processed with CPRammet for wet deposition to produce the necessary extended ISCST3 variables. Values for surface roughness, albedo, Bowen ratio (average moisture), Monin-Obukhov length, and net radiation absorbed at the ground were derived from the June 1999 PCRammet User's Guide. For values where the specific land use type was required (i.e., surface roughness, albedo, and average moisture Bowen ratio), the Grassland land use category was chosen and averaged over the 4 seasonal values provided to arrive at a single annual value for input into CPRammet. For the Monin-Obukhov length, the Open Agricultural land use type and subsequent 2 meter value was used. For the net radiation absorption value, the rural value of 0.15 was chosen. As indicated in the user's guide, anthropogenic heat flux was assumed to be zero for areas outside highly urbanized locations.

5.3.7 Project Emissions

The worst-case representative stack parameters and pollutants emission rates at 100% operating load were used in the CALPUFF analyses. This was accomplished by representing the 100% operating load with a worst-case set of stack parameters and pollutant emission rates that were conservatively selected from performance data over a range of ambient temperatures (i.e., 26, 59, 73, and 105° F) to produce worst-case plume dispersion conditions (i.e., lowest exhaust temperature and exit velocity and the highest emission rate). This process is referred to as "enveloping".

Those pollutants modeled include NO_x, PM/PM₁₀ (filterable and condensable), SO₂, and SO₄ (from (NH₄)₂SO₄). Table 5-2 contains the stack parameters and emission rates modeled in CALPUFF. Furthermore, per guidance from NPS, the PM/PM₁₀ emissions were speciated based on size and composition and therefore were broken into the following constituents: elemental carbon (EC), organic carbon (OC), and soils

(SOIL) for the regional haze analysis. Specifically, guidance from NPS on particulate matter speciation was found in the Emissions & Control Technology area of their website. Per NPS, for natural gas fired combustion turbines, all the filterable portion of PM/PM₁₀ emissions are considered EC and all non-(NH₄)₂SO₄ condensibles are considered to be OC. For fuel oil fired combustion turbines, half of all filterable PM/PM₁₀ are considered EC, half of all filterable PM/PM₁₀ are considered SOIL, and all non-(NH₄)₂SO₄ condensible PM/PM₁₀ are considered OC.

The EC, OC, and SOIL emissions were further speciated based on size. Per NPS guidance, all particles were assumed to be one micron or less for combustion turbines. Table 5-3 presents size distribution for EC, OC, and SOIL particulates as recommended by NPS along with the Project's emission rates for each category and size.

Table 5-2
Stack Parameters and Pollutant Emissions
Used in CALPUFF Modeling Analysis

	Stack Height	Stack Diameter	Exit Velocity	Exit Temp	Pollutant Emission Rate (lb/h)			h)	
Fuel ^(a)	(ft)	(ft)	(ft/s)	(°F)	NO _x	SO ₂	PM/PM ₁₀ ^(b)	SO ₄ (c)	$PM/PM_{10}^{(d)}$
NG	170	18	58.0	166.0	17.50	13.64	38.00	5.39	30.59
FO	170	18	68.0	249.0	81.10	6.29	52.00	3.42	47.31

⁽a)NG - Natural Gas, FO - Ultra Low Sulfur Fuel Oil.

NG: 38.00 lb/hr - 7.41 lb/hr of (NH₄)₂SO₄ = 30.59 lb/hr (3.854 g/s).

FO: $52.00 \text{ lb/hr} - 4.70 \text{ lb/hr} \text{ of } (NH_4)_2SO_4 = 47.31 \text{lb/hr} (5.961 \text{ g/s}).$

⁽b)PM/PM₁₀ represents both front and back half emissions including condensable (NH₄)₂SO₄. Used when comparing PM/PM₁₀ impacts to Class I SILs.

⁽c) Represents the SO₄ portion of (NH₄)₂SO₄ emissions for the scenario that produced the maximum PM/PM₁₀ emissions.

^(d)Represents the portion of PM/PM₁₀ available for speciation based on size and composition. Values derived by subtracting the $(NH_4)_2SO_4$ emissions from the PM/PM₁₀ values.

	Particle Size Distribution							
				Emission Rate (g/s) (a)				
Species	Geometric Mean Diameter	Size Distribution	Non-(NH ₄) ₂ SO ₄ Filterable Condensible Filterable		Non-(NH ₄) ₂ SO ₄ Condensible			
Name	(mm)	(%)	NG EC	NG OC	FO EC	FO SOIL	FO OC	
PM0P05	0.05	15	0.268	0.310	0.213	0.213	0.469	
PM0P10	0.10	25	0.447	0.516	0.354	0.354	0.781	
PM0P15	0.15	23	0.412	0.475	0.326	0.326	0.718	
PM0P20	0.20	15	0.268	0.310	0.213	0.213	0.469	
PM0P25	0.25	11	0.197	0.227	0.156	0.156	0.344	
PM1P00	1.00	11	0.197	0.227	0.156	0.156	0.344	
Sub-Total	-Total 1.789 2.065 1.418 1.418			1.418	3.125			
Total	Total 3.854 5.961							

Table 5-3

5.3.8 CALPUFF Analyses

(a)NG - Natural Gas, FO - Ultra Low Sulfur Fuel Oil.

The preceding model inputs and settings for the CALPUFF modeling system were used to complete the Class I analyses on the ENP and CWA, including regional haze, deposition, and Class I SILs.

5.3.8.1 Regional Haze Analysis. A regional haze analysis was performed for the ENP and CWA for ammonium sulfates, ammonium nitrates, and particulate matter by appropriately characterizing model predicted outputs of SO₄, NO₃, EC, OC, and SOIL concentrations.

Visibility

Visibility is an AQRV for the ENP and CWA. Visibility can take the form of plume blight for nearby areas, or regional haze for long distances (e.g., distances beyond 50 km). Because both the ENP and CWA lie beyond 50 km from the proposed project, the change in visibility is analyzed as regional haze. Regional haze impairs visibility in all directions over a large area by obscuring the clarity, color, texture, and form of what is seen. Current regional haze guidelines characterize a change in visibility by either of the following methods:

- Change in the visual range, defined as the greatest distance that a large dark object can be seen, or
- Change in the light-extinction coefficient (b_{ext}).

Visual range can be related to extinction with the following equation:

$$b_{ext}(Mm^{-1}) = 3912 / vr(Mm^{-1})$$

Visual range (vr) is a measure of how far away a large black object can be seen in the atmosphere under several severe assumptions including: an absolutely dark target, uniform lighting conditions (cloud free skies), uniform extinction in all directions, a limiting contrast discrimination level, a target high enough in elevation to account for earth curvature, and several other factors. Visual range is, at best, a limited concept that allows relatively simple comparisons between visual air quality levels and should not be thought of as the absolute distance that can be seen through the atmosphere.

The b_{ext} is the attenuation of light per unit distance due to the scattering (light reduced away from the site path) and absorption (light captured by aerosols and turned into heat energy) by gases and particles in the atmosphere. A change in the extinction coefficient produces a perceived visual change that is measured by a visibility index called the deciview. The deciview (dv) is defined as:

$$dv = 10 \ln \left(1 + b_{\text{exts}} / b_{\text{extb}}\right)$$

where:

b_{exts} = the extinction coefficient calculated for the source, and

 b_{extb} = the background extinction coefficient

A uniform incremental change in b_{extb} or visual range does not necessarily result in uniform changes in perceived visual air quality. In fact, perceived changes in visibility are best related to a percent change in extinction. Based on NPS guidance, if the change in extinction is less than 5 percent, no further analysis is required. An index similar to the deciview that simply quantifies the percent change in visibility due to the operation of a source is calculated as:

$$\Delta$$
 percent = $(b_{\text{exts}} / b_{\text{extb}}) \times 100$

Background Visual Ranges and Relative Humidity Factors

The background visual range and seasonal relative humidity factor were based on data representative of historical conditions at both the ENP and CWA, respectively. The

background visual ranges, or constituents thereof, for both the ENP and CWA were obtained from the Phase I FLAG Report, December 2000.

Regional Haze Methodology

As provided for in the FLAG document, regional haze was calculated using Method 6, which consists of computing extinctions from speciated PM measurements using FLAG relative humidity adjustment factors applied to observed and modeled sulfate and nitrates. While this process occurs within CALPOST, a typical calculation methodology is illustrated below.

Calculation

Refined impacts will be calculated as follows:

- Obtain 24 hour SO₄, NO₃, EC, OC, and SOIL impacts, in units of micrograms per cubic meter (μg/m³).
- 2. Convert the SO_4 impact to $(NH_4)_2SO_4$ by the following formula:

 $(NH_4)_2SO_4$ (µg/m³) = SO_4 (µg/m³) x molecular weight (NH₄)₂SO₄ / molecular weight SO₄

$$(NH_4)_2SO_4 (\mu g/m^3) = SO_4 (\mu g/m^3) \times 132/96 = SO_4 (\mu g/m^3) \times 1.375$$

Convert the NO₃ impact to NH₄NO₃ by the following formula:

 NH_4NO_3 (µg/m³) = NO_3 (µg/m³) x molecular weight NH_4NO_3 / molecular weight NO_3

$$NH_4NO_3 (\mu g/m^3) = NO_3 (\mu g/m^3) \times 80/62 = NO_3 (\mu g/m^3) \times 1.29$$

3. Compute b_{exts} (extinction coefficient calculated for the source) with the following formula:

$$b_{exts} = 3 \times NH_4NO_3 \times f(RH) + 3 \times (NH_4)_2SO_4 \times f(RH) + 10 \times EC + 4 \times OC + 1 \times SOIL$$

4. Compute b_{extb} (background extinction coefficient) using the background visual range (km) from the FLAG document with the following formula:

$$b_{extb} = 3.912 / Visual range (km)$$

5. Compute the change in extinction coefficients:

in terms of deciviews:

$$dv = 10 \ln (1 + b_{exts}/b_{extb})$$

in terms of percent change of visibility:

$$\Delta$$
 percent = $(b_{exts} / b_{extb}) \times 100$

Based on the predicted SO₄, NO₃, and EC, OC, and SOIL concentrations, the proposed Project's emissions were compared to a 5 percent change in light extinction of the background levels. This is equivalent to a change in deciview of 0.5. As illustrated in Table 5-5, the regional haze results, reported as the maximum value occurring anywhere on the respective receptor rings for each Class I area, are less than the 5 percent

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change in extinction threshold for both the ENP and the CWA and, as such, no further analysis is necessary.

Table 5-5 Regional Haze Results					
	Change in E	Recommended Threshold			
Class I Area	Natural Gas	Fuel Oil	(%)		
Chassahowitzka WA	1.23	1.94	5		
Everglades NP	1.80	2.76	5		

^(a)Change in extinction was compared against the natural conditions presented in the FLAG 2000 document.

5.3.8.2 Deposition Analyses. Deposition analyses were performed for ENP and CWA for both total sulfur and total nitrogen. The analyses followed those procedures and methodologies set forth in the IWAQM Phase II Report and the *Guide for Applying the EPA Class I Screening Methodology with the CALPUFF Modeling System* document, developed by Earth Tech, Inc. (the model developers) in September 2001. This document is a guide for using the POSTUTIL processor to perform deposition analyses. Specifically, deposition analyses were performed as follows:

- Perform CALPUFF model runs using the specified options previously mentioned (including output of both dry and wet deposition).
- Use POSTUTIL to combine the wet and dry flux output files from CALPUFF and scale the contributions of SO₂, SO₄, NO_x, NO₃, and HNO₃ such that total (i.e., wet and dry) nitrogen and total sulfur flux are contained in the same file. The POSTUTIL file is set up such that SO₂ and SO₄ contribute sulfur mass, and SO₄, NO_x, HNO₃, and NO₃ contribute to the nitrogen mass.
- Apply the appropriate scaling factors found in the IWAQM Phase II
 Report (Section 3.3, Deposition Calculations) to the CALPOST runs to
 account for the conversion of grams to kilograms, square meters to
 hectares (ha), seconds to hours, and hours to a year. Thus, the CALPOST
 results are in kg/ha/yr.

The model-predicted results were compared to the 0.01 kg/ha/year Deposition Analysis Threshold (DAT) developed jointly by the NPS and the U.S. Fish and Wildlife Service (FWS). The results of the deposition analysis for each of the Class I areas are presented Table 5-6 and represent the highest impact occurring anywhere on the respective receptor rings for each Class I area. As illustrated in the table, the deposition results for both the ENP and the CWA are less than the 0.01 DAT and, as such, no further analysis is necessary.

Table 5-6 Deposition Results					
	Depos	litrogen sition ^(a) na/yr)	Total Depos (kg/l	Deposition Analysis	
Class I Area	NG FO NG FO				Threshold ^(c)
Chassahowitzka WA	2.3E-4 6.5E-4		3.7E-4	1.8E-4	0.01
Everglades NP	3.3E-4	9.7E-4	5.1E-4	2.6E-4	0.01

⁽a)Includes both wet and dry deposition with SO₄, NO_x, HNO₃, and NO₃ contributing to the nitrogen mass.

5.3.8.3 Class I Impact Analysis. Ground-level impacts (in $\mu g/m^3$) at the ENP and CWA were calculated for NO_x , SO_2 , and PM/PM_{10} criteria pollutants for each applicable averaging period. The results of this analysis were compared with the Class I Significant Impact Levels (SILs) calculated as 4 percent of the Class I Increment values. Table 5-7 presents the maximum results of the Class I analysis for the 5 year period that was modeled. As illustrated in the table, there are no impacts above the Class I SILs at either the ENP or the CWA and, as such, no further analysis is necessary.

⁽b) Includes both wet and dry deposition with SO₂ and SO₄ contributing sulfur mass.

⁽c) For all areas east of the Mississippi River.

	Cla	Table ass I Significant Impact Lev		ults	
	Averaging	Model-Predic (μg/		PSD Class I SIL ^(b)	Exceed
Pollutant	Period	Natural Gas	Fuel Oil	(μg/m³)	SIL?
Chassahow	itzka Wilderne	ess Area			
NO _x	Annual	6.90E-5	3.15E-4	0.10	NO
	Annual	2.64E-4	1.21E-4	0.08	NO
SO ₂	SO ₂ 24 Hour	5.95E-3	2.56E-3	0.20	NO
	3 Hour	1.61E-2	7.15E-3	1.0	NO
PM/PM ₁₀	Annual	1.04E-3	1.39E-3	0.16	NO
FIVI/FIVI ₁₀	24 Hour	2.70E-2	3.50E-2	0.32	NO
Everglades	National Park				
NO _x	Annual	2.53E-4	1.12E-3	0.10	NO
	Annual	5.37E-4	2.42E-4	0.08	NO
SO ₂	24 Hour	1.01E-2	4.41E-3	0.20	NO
	3 Hour	3.35E-2	1.46E-2	1.0	NO
PM/PM ₁₀	Annual	1.92E-3	2.55E-3	0.16	NO
LIAN LIAI 10	24 Hour	4.05E-2	5.27E-2	0.32	NO

⁽a) Model-predicted impacts are for the 5 year period that was in the analysis: 1987, 1988, 1989, 1990, and 1991. (b) Class I Significant Impact Levels are calculated as 4 percent of the PSD Class I Increment values.

Appendix A Emission Calculation Spreadsheet

FMPA Treasure Coast Energy Center Combined Cycle Unit 1 Project 138859 Potential to emit analysis Combustion Turbine Unit 1 GE PG7241 data Prepared by: Black & Veatch

CT performance data at average ambient temperature (73°F) and 100% load Calculations based on 12/15/04 performance runs. Natural gas sulfur content of 2 grains per 100 scf. ULS fuel oil sulfur content of 0.0015 percent.

Operational restrictions: natural gas firing

fuel oil firing

8760 hours per year 500 hours per year

	Combined Cy	cle Operation v	vith Duct Burn	er and SCR	_			1	
	Natural	Gas Fired	Fuel C	Oil Fired	Potential to			i	
	Hourty Emission Rate - Case 5s	Potential to	Hourty Emission Rate - Case 6a	Potential to Emit	Emit on a Maximum Pollutant by Pollutant Basis	P SD SEL	PSD Major Modification	Natural Gas Fired - Max Emission Rate	
Pollutant	(lb/hour)	(tpy)	(lb/hour)	(tpy)	(tpy)	(tpy)	(Yes/No)	(lb/hour)	(ib/hour)
NO _x	16.5	72.3	76.0	19.0	87.1	40	Yes	17.5	81.1
co	50.1	219.4	86.2	21.6	228.5	100	Yes	52.3	92.4
PM (front half)	14.5	63.5	22.5	5.6	65.5	25	Yes	14.7	22.5
PM ₁₀ (front half)	14.5	63.5	22.5	5.6	65.5	15	Yes	14.7	22.5
PM (front and back half)	38.0	166.4	49.9	12.5	169.4	25	Yes	38	52
PM ₁₀ (front and back half)	38.0	168.4	49.9	12.5	169.4	15	Yes	38	52
SO ₂ (a)	12.9	56.5	6.04	1.5	` 56.5	40	Yes	13.6	6.3
VOC	5.0	21.9	9.7	2.4	23.1	40	No	5.1	10.2
H ₂ SO ₄ mist ⁽⁰⁾	5.12	22.4	1.95	0.5	22.4	7	Yes	6.06	3.49

 $^{^{\}rm (a)}$ SO2 emissions do not include the effect of SO2 oxidation to SO3.

⁽b) H₂SO₄ based on SO₂ to SO₃ oxidation effects and 100% of SO₃ is converted to H₂SO₄.

Treasure Coast Energy Center Combined Cycle Unit 1 Project 138859

Potential to emit analysis Auxiliary Boiler

Prepared by: Black & Veatch

Operational restrictions:

Auxiliary boiler operation

8760 hours per year

Auxiliary Boiler Emissions					
Pollutant	Hourly Emission Rate (lb/hour)	Potential to Emit (tpy)			
NO _x	0.260	1.14			
СО	0.520	2.28			
PM/PM ₁₀	0.029	0.13			
SO ₂ ^(a)	0.040	0.18			
VOC	0.040	0.18			

 $^{^{(}a)}$ SO₂ emissions are calculated based on the boiler heat input rate of 7.2 mmBtu/hr, assuming a natural gas heating value of 1,020 mmBtu/mmscf and a natural gas sulfur content of 2 grains per 100 scf.

FMPA Treasure Coast Energy Center Combined Cycle Unit 1 Project 138859 Potential to emit analysis Fire Pump Diesel Engine Prepared by: Black & Veatch

Operational restrictions: Fire pump diesel engine projected operation

200 hours per year

Fire Pump Diesel Engine Emissions					
	Hourly Emission Rate	Potential to Emit			
Pollutant	(lb/hour)	(tpy)			
NO _x	5.879	0.59			
CO	1.225	0.12			
PM/PM ₁₀	0.113	0.01			
SO ₂	0.003	0.00			
VOC	0.213	0.02			

^{*} Emission specs are for a Clarke Detroit Diesel - Allison Model DDFP-T6FA unit.

FMPA Treasure Coast Freem

Treasure Coast Energy Center Combined Cycle Unit 1 Project 138859

Potential to emit analysis Safe Shutdown Generator Prepared by: Black & Veatch

Operational restrictions: Safe Shutdown Generator Projected Operation

200 hours per year

Safe Shutdown Generator Emissions					
Pollutant	Hourly Emission Rate (lb/hour)	Potential to Emit (tpy)			
NO _x	11.253	1.13			
CO	0.891	0.09			
PM/PM ₁₀	0.077	0.01			
SO ₂ (a)	0.008	0.00			
VOC	0.110	0.01			

^{*} Emission specs are for a Caterpillar Engine

⁽a) SO_2 emission rates are based on a fuel consumption rate of 36.3 gal/hr (vendor information), a fuel density of 7.05 lb/gal (AP-42 Appendix A), and a fuel oil sulfur content of 0.0015 percent by weight.

Treasure Coast Energy Center **Combined Cycle Unit 1 Project** 138859

Potential to emit analysis Cooling Tower PM₁₀ Emissions Prepared by: Black & Veatch

Cooling Tower Parameters

Given:

Circulating Flow Rate Circulating Water TDS

Drift Percent

Annual Operational Hours

111,130 gpm 3,918 ppm 0,0005 % 8760 hrs

Requested:

Particle Size

10.0 microns

Calculated:

% Mass Less Than 10 microns

39.138 % 4.77 tpy

PM Emissions Rate

PM10 Emission Rate

1.87 tpy

		EPRI Drift	Spectrum		
	-:		Solid	Solid	EPRI %
Droplet	Droplet		Particulate	Particulate	Mass
Size	Volume	Droplet	Volume	Diameter	Percent
(um)	(um3)	Mass (ug)	(um3)	(um)	Smaller
10	5.24E+02	5.24E-04	9.32E-01	1.212	0.000
20	4.19E+03	4.19E-03	7.46E+00	2.424	0.196
30	1.41E+04	1.41E-02	2.52E+01	3.636	0.226
40	3.35E+04	3.35E-02	5.97E+01	4.848	0.514
50	6.54E+04	6.54E-02	1.17E+02	6.061	1.816
60	1.13E+05	1.13E-01	2.01E+02	7.273	5.702
70	1.80E+05	1.80E-01	3.20E+02	8.485	21.348
90	3.82E+05	3.82E-01	6.80E+02	10.909	49.812
110	6.97E+05	6.97E-01	1.24E+03	13.333	70.509
130	1.15E+06	1.15E+00	2.05E+03	15.758	82.023
150	1.77E+06	1.77E+00	3.15E+03	18.182	88.012
180	3.05E+06	3.05E+00	5.44E+03	21.818	91.032
210	4.85E+06	4.85E+00	8.64E+03	25.455	
240	7.24E+06	7.24E+00	1.29E+04	29.091	94.091
270	1.03E+07	1.03E+01	1.84E+04	32.727	94.689
300	1.41E+07	1.41E+01	2.52E+04	36.364	96.288
350	2.24E+07	2.24E+01	4.00E+04	42.424	97.011
400		3.35E+01	5.97E+04	48.485	
450	4.77E+07	4.77E+01	8.50E+04	54.545	99.071
500	6.54E+07		1.17E+05	60.606	99.071
600	1.13E+08	1.13E+02	2.01E+05	72.727	100.000
Source:			-		

"Calculating Realistic PM10 Emissions from Cooling Towers." Joel Reisman and Gordon Frisbie. Abstract No. 216. Air & Waste Management Association 94th Annual Conference and Exhibition in Orlando, FL, June 25-28, 2001.

Interpolation to Find	Required \	/alue						
Given Values:	Given Values: 8.485 21.348							
	10.909	49.812						
Interpolated Value:	10	39.138						

Treasure Coast Energy Center Combined Cycle Unit 1 Project 138859

Potential to emit analysis Cooling Tower PM Emissions Prepared by: Black & Veatch

Cooling Tower Parameters

Given:

Circulating Flow Rate Circulating Water TDS

Drift Percent

Annual Operational Hours

111,130 gpm 5,331 ppm 0.0005 % 8760 hrs

Requested:

Particle Size

10.0 microns

Calculated:

% Mass Less Than 10 microns

27.683 % 6.49 tpy

PM Emissions Rate

PM10 Emission Rate

1.80 tpy

	EPRI Drift Spectrum					
			Solid	Solid	EPRI %	
•	Droplet	l	Particulate	Particulate	Mass	
Size	Volume	Droplet	Volume	Diameter	Percent	
(um)	(um3)	Mass (ug)	(um3)	(um)	Smaller	
10	5.24E+02	5.24E-04	1.27E+00	1.343	0.000	
20	4.19E+03	4.19E-03	1.02E+01	2.686	0.196	
30	1.41E+04	1.41E-02	3.43E+01	4.029	0.226	
40	3.35E+04	3.35E-02	8.12E+01	5.373	0.514	
50	6.54E+04	6.54E-02	1.59E+02	6.716	1.816	
60	1.13E+05	1.13E-01	2.74E+02	8.059	5.702	
70	1.80E+05	1.80E-01	4.35E+02	9.402	21.348	
90	3.82E+05	3.82E-01	9.25E+02	12.088	49.812	
110	6.97E+05	6.97E-01	1.69E+03	14.775	70.509	
130	1.15E+06	1.15E+00	2.79E+03	17.461	82.023	
150	1.77E+06	1.77E+00	4.28E+03	20.147	88.012	
180	3.05E+06	3.05E+00	7.40E+03	24.177	91.032	
210	4.85E+06	4.85E+00	1.18E+04	28.206	92.468	
240	7.24E+06	7.24E+00	1.75E+04	32.236	94.091	
270	1.03E+07	1.03E+01	2.50E+04	36.265	94.689	
300	1,41E+07	1.41E+01	3.43E+04	40.295	96.288	
350	2.24E+07	2.24E+01	5.44E+04	47.011	97.011	
400	3.35E+07	3.35E+01	8.12E+04	53.727	98.340	
450	4.77E+07	4.77E+01	1.16E+05	60.442	99.071	
500	6.54E+07	6.54E+01	1.59E+05	67.158		
600	1.13E+08	1.13E+02	2.74E+05	80.590	100.000	
C						

"Calculating Realistic PM10 Emissions from Cooling Towers." Joel Reisman and Gordon Frisbie. Abstract No. 216. Air & Waste Management Association 94th Annual Conference and Exhibition in Orlando, FL, June 25-28, 2001.

Interpolation to Find	Interpolation to Find Required Value		
Given Values:	9.402 12.088	21.348 49.812	
interpolated Value:	10	27.683	

Treasure Coast Energy Center Combined Cycle Unit 1 Project 138859

Potential to emit analysis Diesel Fuel Storage Tank Emissions Prepared by: Black & Veatch

BASED ON EPA TANKS PROGRAM

Average CT fuel oil use (lb/hr)
Fuel oil density (lb/gal)
Annual fuel oil use (hr/yr)
Annual tank throughput (gal/year)
VOC emission rate from TANKS (tpy)

96540 From performance data 7.05 From AP-42 Appendix A. 500 Permitting basis 6,846,809

0.16

Treasure Coast Energy Center Combustion Turbine Unit 1 Project 138859

Potential to emit analysis
Total Project Emissions
Prepared by: Black & Veatch

Pollutant	Potential to Emit (tpy)	PSD SEL (tpy)	PSD Major Modification (Yes/No)
NO _x	90.0	40	YES
CO	231.0	100	YES
РМ	176.1	25	YES
PM ₁₀	171.4	15	YES
SO₂	56.6	40	YES
VOC*	23.4	40	NO
H₂SO₄ mist	22.4	7	YES

Treasure Coast Energy Center Combined Cycle Unit 1 Project 138859

Hazardous Air Pollutant (HAP) Emission Estimates
Combustion Turbine Unit 1 - Distillate Oil Firing

GE PG7241 data Prepared by: Black & Veatch

FUEL: HEAT INPUT (MMBtu/hr): HOURS OF OPERATION: NUMBER OF TURBINES		DISTILLATE OIL (1881.5 (600		
	DISTILLATE OIL	FIRED TURBINE EMISSION		
Pollutant	Emission factor ⁽¹⁾ Ib/MMBtu	Emissions lb/hr/turbine	Emissions tons/yr	
1.3 Butadiene	1.60E-05	3.01E-02	0.008	
Benzene	5.50E-05	1.03E-01	0.026	
Formaldehyde	2.80E-04	5.27E-01	0.132	
Naphthalene	3.50E-05	6.59E-02	0.016	
PAH	4.00E-05	7.53E-02	0.019	
	Total On	ganic HAP Emissions (tpy)	0.200	
Pollutant		ganic HAP Emissions (tpy) URBINE METALLIC HAP E Emissions		
Pollutant	DISTILLATE OIL FIRED T	URBINE METALLIC HAP E	MISSIONS	
	DISTILLATE OIL FIRED T Emission factor ⁽²⁾ Ib/MMBtu	URBINE METALLIC HAP E Emissions Ib/hr/turbine	MISSIONS Emissions tons/yr	
Arsenic	DISTILLATE OIL FIRED T Emission factor ⁽²⁾ Ib/MMBtu 1.10E-05	URBINE METALLIC HAP E Emissions Ib/hr/turbine 2.07E-02	MISSIONS Emissions tons/yr	
Arsenic Beryllium	DISTILLATE OIL FIRED T Emission factor ⁽²⁾ Ib/MMBtu 1.10E-05 3.10E-07	URBINE METALLIC HAP E Emissions Ib/hr/turbine 2.07E-02 5.83E-04	Emissions tons/yr 0.005 0.000	
Arsenic Beryllium Cadmium	DISTILLATE OIL FIRED T Emission factor ⁽²⁾ Ib/MMBtu 1.10E-05 3.10E-07 4.80E-06	URBINE METALLIC HAP E Emissions Ib/hr/turbine 2.07E-02 5.83E-04 9.03E-03	Emissions tons/yr 0.005 0.000 0.002	
Arsenic Beryllium Cadmium Chromium	DISTILLATE OIL FIRED T Emission factor ⁽²⁾ Ib/MMBtu 1.10E-05 3.10E-07 4.80E-06 1.10E-05	URBINE METALLIC HAP E Emissions Ib/hr/turbine 2.07E-02 5.83E-04 9.03E-03 2.07E-02	MISSIONS Emissions tons/yr 0.005 0.000 0.002 0.005	
Arsenic Beryllium Cadmium Chromium Lead	DISTILLATE OIL FIRED T Emission factor ⁽²⁾ Ib/MMBtu 1.10E-05 3.10E-07 4.80E-06 1.10E-05 1.40E-05	URBINE METALLIC HAP E Emissions Ib/hr/turbine 2.07E-02 5.83E-04 9.03E-03 2.07E-02 2.63E-02	MISSIONS Emissions tons/yr 0.005 0.000 0.002 0.005 0.005	
Arsenic Beryllium Cadmium Chromium Lead Manganese	DISTILLATE OIL FIRED T Emission factor ⁽²⁾ Ib/MMBtu 1.10E-05 3.10E-07 4.80E-06 1.10E-05 1.40E-05 7.90E-04	URBINE METALLIC HAP E Emissions Ib/hr/turbine 2.07E-02 5.83E-04 9.03E-03 2.07E-02 2.63E-02 1.49E+00	MISSIONS Emissions tons/yr 0.005 0.000 0.002 0.005 0.005 0.007 0.372	
Arsenic Beryllium Cadmium Chromium Lead Manganese Mercury	DISTILLATE OIL FIRED T Emission factor ⁽²⁾ Ib/MMBtu 1.10E-05 3.10E-07 4.80E-06 1.10E-05 1.40E-05 7.90E-04 1.20E-08	URBINE METALLIC HAP E Emissions Ib/hr/turbine 2.07E-02 5.83E-04 9.03E-03 2.07E-02 2.63E-02 1.49E+00 2.26E-03	MISSIONS Emissions tons/yr 0.005 0.000 0.002 0.005 0.007 0.372 0.001	
Arsenic Beryllium Cadmium Chromium Lead Manganese	DISTILLATE OIL FIRED T Emission factor ⁽²⁾ Ib/MMBtu 1.10E-05 3.10E-07 4.80E-06 1.10E-05 1.40E-05 7.90E-04	URBINE METALLIC HAP E Emissions Ib/hr/turbine 2.07E-02 5.83E-04 9.03E-03 2.07E-02 2.63E-02 1.49E+00	MISSIONS Emissions tons/yr 0.005 0.000 0.002 0.005 0.005 0.007 0.372	

Heat Input rate is at 100% load and average site ambient temperatures.

Summary o	of HAP Emissions		
Pollutant Emissions			
	(tons per year)		
1.3 Butadiene	0.008		
Benzene	0.026		
Formaldehyde	0.132		
Naphthalene	0.016		
PAH	0.019		
Arsenic	0.005		
Beryllium	0.000		
Cadmium	0.002		
Chromium	0.005		
Lead	0.007		
Manganese	0.372		
Mercury	0.001		
Nickel	0.002		
Selenium	0.012		
Total HAPs	0.606		

⁽¹⁾ Emission factors from AP-42 Section 3.1 Table 3.1-4. (2) Emission factors from AP-42 Section 3.1 Table 3.1-5.

Treasure Coast Energy Center Combined Cycle Unit 1 Project 138859

Hazardous Air Pollutant (HAP) Emission Estimates

Combustion Turbine Unit 1 - Natural Gas Firing

GE PG7241 data

Prepared by: Black & Veatch

FUEL: HEAT INPUT (MMBtu/hr): HOURS OF OPERATION: NUMBER OF TURBINES		NATURAL GAS 1722:5 .8760 .1 ED TURBINE ORGANIC HAP EMISSIONS	
Pollutant	Emission factor ⁽¹⁾ ib/MMBtu	Emissions Ib/hr/turbine	Emissions tons/yr
1,3 Butadiene	4.30E-07	7.41E-04	0.003
Acetaldehyde	4.00E-05	6.89E-02	0.302
Acrolein	6.40E-06	1.10E-02	0.048
Benzene	1.20E-05	2.07E-02	0.091
Ethylbenzene	3.20E-05	5.51E-02	0.241
Formaldehyde	7.10E-04	1.22E+00	5.357
Naphthalene	1.30E-06	2.24E-03	0.010
PAH	2.20E-06	3.79E-03	0.017
Propylene Oxide	2.90E-05	5.00E-02	0.219
Toluene	1.30E-04	2.24E-01	0.981
Xylenes	6.40E-05	1.10E-01	0.483

⁽¹⁾ Emission factors from AP-42 Section 3.1 Table 3.1-3. Heat Input rate is at 100% load and average site ambient temperatures.

Summary of HAP Emissions			
Pollutant	Emissions (tons per year)		
1,3 Butadiene	0.003		
Acetaldehyde	0.302		
Acrolein	0.048		
Benzene	0.091		
Ethylbenzene	0.241		
Formaldehyde	5.357		
Naphthalene	0.010		
PAH	0.017		
Propylene Oxide	0.219		
Toluene	0.981		
Xylenes	0.483		
Total HAPs	7.751		

FMPA
Treasure Coast Energy Center
Combined Cycle Unit 1 Project
138859
Hazardous Air Pollutant (HAP) Emission Estimates
Combustion Turbine Unit 1 - Totals
GE PG7241 data

Prepared by: Black & Veatch

Summary of HAP Emissions		
Pollutant	Emissions (tons per year	
1,3 Butadiene	0.011	
Acetaldehyde	0.302	
Acrolein	0.048	
Benzene	0.111	
Ethylbenzene	0.241	
Formaldehyde	5.357	
Naphthalene	0.026	
PAH	0.034	
Propylene Oxide	0.219	
Toluene	0.981	
Xylenes	0.483	
Arsenic	0.005	
Beryllium	0.000	
Cadmium	0.002	
Chromiuim	0.005	
Lead	0.007	
Manganese	0.372	
Mercury	0.001	
Nickel	0.002	
Selenium	0.012	
Total HAPs	7.914	

FMPA
Treasure Coast Energy Center
Combined Cycle Unit 1 Project
138859
Hazardous Air Pollutant (HAP) Emission Estimates
Combustion Turbine Unit 1 - Duct Burner
Prepared by: Black & Vestch

FUEL: HEAT INPUT (MMBbuhr): MATIBAL CAS MEATING VALUE (MMRhyMMbch NATURAL GAS

HOURS OF OPERATION: NUMBER OF DUCT BURNERS		(1620 (6780		
NATURA	L GAS CONBUSTION ORGA	NIC HAP EMISSIONS		
Pollutent	Emission factor ⁽¹⁾	Emissions	Emissions	
	lb/MMscf	Do/har	tons/yr	
2-Mothylmaphthalene	2.40E-05	1,30E-05	5.712E-05	
3-Methylchioranthrene	1.80E-06	9.78E-07	4.284E-06	
7,12-Dimethylbenz(a)anthracene	1.60E-05	8.69E-08	3.808E-05	
Acenaphthene	1.60E-06	9.78E-07	4.284E-06	
Acenaphthylene	1.60E-06	9.78E-07	4.284E-08	
Anthracene	2.40E-06	1.30E-06	5.712E-08	
Benz(a)antivacene	1.80E-08	9.78E-07	4.284E-08	
Benzene	2.10E-03	1.14E-03	4.998E-03	
Benzo(a)pyrene	1.20E-08	6.52E-07	2.856E-06	
Berrzo(b)fluoranthene	1.80E-06	9.78E-07	4.284E-06	
Bertzo(g,h,l)perylene	1.20E-06	6.52E-07	2.856E-08	
Benzo(k)fluoranthene	1.80E-06	9.78E-07	4.284E-08	
Chrysene	1.60E-06	9.78E-07	4.284E-08	
Dibenzo(a,h)anthracene	1,20E-08	6.52E-07	2.856E-06	
Dichlorobenzene	1.20E-03	6.52E-04	2.856E-03	
Fluoranthene	3.00E-06	1.63E-08	7.139E-06	
Fluorene	2.80E-06	1.52E-06	6.663E-06	
Formaldehyde	7.50E-02	4.08E-02	1.785E-01	
Hexane	1.80E+00	_ 9.78E-01	4.284E+00	
ndeno(1,2,3-od)pyrene	1.80E-06	9.78E-07	4.284E-06	
Naphthalene	6.10E-04	3.31E-04	1.452E-03	
Phonanatireno	1.70E-05	9.24E-06	4.048E-05	
Pyrene	5.00E-06	2.72E-06	1,190E-05	
Toluene	3.40E-03	1.85E-03	8.091E-03	
	Total Organ	NIC HAP Emissions (tpy)	4.480E+00	
Pollutent	Emission factor ⁽²⁾	Emissions	Emissions	
	th/MMBtu	lb/hr/turbine	tons/vr	
Arsenic	2.00E-04	1.09E-04	4.76E-04	
Beryllium	1.20E-05	6.52E-06	2.86E-05	
	1.10E-03	5.98E-04	2.62E-03	
Cadmium				
	1.40E-03	7.61E-04	3.33E-03	
Chromium	1.40E-03 8.40E-05	7.51E-04 4.56E-05	3.33E-03 2.00E-04	
Cedmium Chromium Cobelt Mansanese				
Chromium Cobelt Manganese	8.40E-05	4.56E-05	2.00E-04	
Chromium	8.40E-05 3.80E-04	4.56E-05 2.06E-04	2.00E-04 9.04E-04	

⁽¹⁾ Emission factors from AP-42 Section 1.4 Table 1.4-3. (2) Emission factors from AP-42 Section 1.4 Table 1.4-4.

Summary of HAP E	nissions	
Pollutant	Emissions	
	(tons per year)	
2-Methylnaphthalene	5.71E-05	
3-Methylchioranthrene	4.28E-06	
12-Dimethylbenz(a)anthracene	3.81E-05	
Acenaphthene	4.28E-06	
Acenaphthylene	4.28E-06	
Andivacene	5.71E-08	
Benz(a)anthracene	4.28E-08	
Benzene	5.00E-03	
Benzo(a)pyrene	2.86E-06	
Benzo(b)fluoranthene	4.28E-06	
Benzo(g,h,i)perylene	2.86E-06	
Benzo(k)fluoranthene	4.28E-06	
Chrysene	4.28E-06	
Dibenzo(a,h)anthracene	2.86E-06	
Dichlorobenzene	2.86E-03	
Fluorenthene	7.14E-06	
luorene	6.66E-06	
ormaldehyde	1.78E-01	
lexane	4.28E+00	
ndeno(1,2,3-cd)pyrene	4.28E-06	
Naphthalene	1.45E-03	
Phenanativene	4.05E-05	
Pyrene	1.19E-05	
Toluene	8.09E-03	
Arsenic	4.75E-04	
Bery©um	2.86E-05	
Cadmium	2.62E-03	
Chromium	3.33E-03	
Cobalt	2.00E-04	
Manganese	9.04E-04	
Mercury	6.19E-04	
Nickel	5.00E-03	
Seleraum	5.71E-05	
Total HAPs	4.49E+00	

FMPA
Treasure Coast Energy Center
Combined Cycle Unit 1 Project
19889
Hazardous Air Pollutant (HAP) Emission Estimates
Audilary Boller
Prepared by: Black & Vestch

FUEL:		NATU	WI GAS
IEAT INPUT (MMBtufur):		1	12
NATURAL GAS HEATING VALUE (MMBb://MMsdf): HOURS OF OPERATION:		1 8	028)
		8	76U
NUMBER OF BOILERS		MC2-14-1-2-2-18-2-2-2-2-2-2-2-2-2-2-2-2-2-2-2-	A 40 C B T 44 C 27 27 28 28 28 28 28 28 28 28 28 28 28 28 28
NATURA	L GAS COMBUSTION OR	GANIC HAP EMISSIONS	
Poliutant	Emission factor ⁽¹⁾	Emissions	Emissions
	lb/MMscf	lb/hr	tons/yr
2-Methylnaphthalene	2.40E-05	1.89E-07	7.42E-07
3-Methylchioranthrene	1.80E-06	1.27E-08	5.57E-08
7,12-Dimethylbenz(a)anthracene	1.60E-05	1.13E-07	4.95E-07
Acenaphthene	1.80E-06	1.27E-08	5.57E-08
Acenaphthylene	1.60E-06	1.27E-08	5.57E-08
Anthracene	2.40E-06	1.69E-08	7.42E-08
Benz(a)anthracene	1.80E-06	1.27E-08	5.57E-08
Benzene	2.10E-03	1.48E-05	6.49E-05
Benzo(a)pyrene	1.20E-06	8.47E-09	3.71E-08
Benzo(b)fluxrasithene	1.80E-06	1.27E-08	5.57E-08
Benzo(g,h,l)perylene	1.20E-06	8.47E-09	3.71E-08
Senzo(k)fluoranthene	1.80E-06	1.27E-08	5.57E-08
Chrysene	1.80E-06	1.27E-08	5.57E-08
Olbenzo(a.h)anthracene	1,20E-06	8,47E-09	3.71E-08
Dichlorobenzene	1,20E-03	8.47E-08	3.71E-05
Rupranthene	3.00E-06	2,12E-08	9.26E-08
lucrene	2.80E-06	1,98E-08	8.66E-08
ormaldehyde	7.50E-02	5.29E-04	2.32E-03
terrane	1.80E+00	1.27E-02	5.57E-02
ndeno(1,2,3-cd)pyrene	1.80E-06	1.27E-08	5.57E-08
Nanhthalene	6.10E-04	4.31E-06	1.69E-05
henanathrene	1.70E-05	1.20E-07	5.26E-07
Vrene	5.00E-08	3.53E-08	1.56E-07
Toluene	3.40E-03	2.40E-05	1.05E-04
	Total Org	enic HAP Emissions (tpy)	5.62 <u>E-02</u>
MATURA	L GAS COMBUSTION ME	TALLIC HAP EMISSIONS	
Pollutant	Emission factor ⁽²⁾	Emissions	Emissions
	BAMMStu	Refer	tons/yr
Arsenic	2.00E-04	1.41E-06	6.18E-06
Bervillum	1.20E-05	8.47E-08	3,71E-07
Cedmium	1.10E-03	7.76E-06	3,40E-05
Chromium	1.40E-03	9.88E-06	4,33E-05
Cobell	8.40E-05	5.93E-07	2.60E-06
Vanganese	3.80E-04	2.68E-06	1.17E-05
Mercury	2.60E-04	1.84E-06	8.04E-06
Wickel	2.10E-03	1.48E-05	6.49E-05
Selenium	2.40E-05	1.69E-07	7.42E-07

⁽¹⁾ Emission factors from AP-42 Section 1.4 Table 1.4-3.
(2) Emission factors from AP-42 Section 1.4 Table 1.4-4.

Summary of HAP E	missions
Pollutant	Emissions
	ftons per year
2-Methytnaphthalene	7.42E-07
3-Methylchlorarthrene	5.57E-08
7,12-Dimethylbenz(a)anthracene	4.95E-07
Acenaphthene	5,57E-08
Acenaphthylene	5.57E-08
Anthracene	7.42E-08
Benz(e)anthracene	5.57E-08
Benzene	6,49E-05
Benzo(a)pyrene	3,71E-08
Benzo(b)fluoranthene	5.57E-08
Benzo(g,h,l)perylene	3.71E-08
Benzo(k)fluoranthene	5.57E-08
Chrysene	5.57E-08
Dibenzo(a,h)anthracene	3.71E-08
Dichlorobenzene	3.71E-05
Fluoranthene	9.28E-08
Fluorene	8.66E-08
Formaldehyde	2.32E-03
texane	5.57E-02
ndeno(1,2,3-cd)pyrene	5.57E-08
Naphthalene	1.89E-05
Phenenathrene	5.26E-07
Pyrene	1.55E-07
Toluene	1.05E-04
Amenic	6.18E-06
Bervilium	3.71E-07
Cedmium	3.40E-05
Chromium	4.33E-05
Cobalt	2.60E-06
Manganese	1.17E-05
Mercury	8.04E-06
Nickel	6.49E-05
Setenium	7.42E-07
Total HAPs	5.84E-02

Treasure Coast Energy Center Combined Cycle Unit 1 Project 138859

Hazardous Air Pollutant (HAP) Emission Estimates

Diesel Engine Fire Pump Prepared by: Black & Veatch

FUEL: HEAT INPUT (MM HOURS OF OPER		2	LATE OIL 274 200
	DIESEL ENGIN	E ORGANIC HAP EMISSION	IS
Pollutant	Emission factor ⁽¹⁾ Ib/MMBtu	Emissions ib/hr	Emissions tons/yr
1,3 Butadiene	3.91E-05	8.89E-05	0.000
Acetaldehyde	7.67E-04	1.74E-03	0.000
Acrolein	9.25E-05	2.10E-04	0.000
Benzene	9.33E-04	2.12E-03	0.000
Formaldehyde	1.18E-03	2.68E-03	0.000
Naphthalene	8.48E-05	1.93E-04	0.000
Toluene	4.09E-04	9.30E-04	0.000
Xylenes	2.85E-04	6.48E-04	0.000
PAH	1.68E-04	3.82E-04	0.000
	Total O	rganic HAP Emissions (tpy)	0.001

⁽¹⁾ Emission factors from AP-42 Section 3.3 Table 3.3-2. Heat input rate is for a Clarke Detroit Diesel - Allison Model DDFP-T6FA unit.

Summary o	f HAP Emissions
Pollutant	Emissions
	(tons per year)
1,3 Butadiene	0.000
Acetaldehyde	0.000
Acrolein	0.000
Benzene	0.000
Formaldehyde	0.000
Naphthalene	0.000
Toluene	0.000
Xylenes	0.000
PAH	0.000
Total HAPs	0.001

Treasure Coast Energy Center Combined Cycle Unit 1 Project 138859

Hazardous Air Pollutant (HAP) Emission Estimates

Safe Shutdown Generator Prepared by: Black & Veatch

FUEL: HEAT INPUT (MM HOURS OF OPER		5	ATE OIL 08 00
	_	E ORGANIC HAP EMISSION	IS
Pollutant	Emission factor ⁽¹⁾ Ib/MMBtu	Emissions ib/hr	Emissions tons/yr
1,3 Butadiene	3.91E-05	1.99E-04	0.000
Acetaldehyde	7.67E-04	3.90E-03	0.000
Acrolein	9.25E-05	4.70E-04	0.000
Benzene	9.33E-04	4.74E-03	0.000
Formaldehyde	1.18E-03	5.99E-03	0.001
Naphthalene	8.48E-05	4.31E-04	0.000
Toluene	4.09E-04	2.08E-03	0.000
Xylenes	2.85E-04	1.45E-03	0.000
PAH	1.68E-04	8.53E-04	0.000
	Total C	Organic HAP Emissions (tpy)	0.002

⁽¹⁾ Emission factors from AP-42 Section 3.3 Table 3.3-2. Heat input rate is for a Caterpillar Engine

of HAP Emissions
Emissions
(tons per year)
0.000
0.000
0.000
0.000
0.001
0.000
0.000
0.000
0.000
0.002

FMPA
Treasure Coast Energy Center
Combined Cycle Unit 1 Project
138859
Hazardous Air Pollutant (HAP) Emission Estimates
Totals
Prepared by: Black & Veatch

Summary of HAP En	nissions
Pollutant	Emissions ⁽¹⁾ (tons per year)
1,3 Butadiene	0.011
2-Methylnaphthalene	0.000
3-Methylchloranthrene	0.000
7,12-Dimethylbenz(a)anthracene	0.000
Acenaphthene	0.000
Acenaphthylene	0.000
Acetaldehyde	0.302
Acrolein	0.048
Anthracene	0.000
Benz(a)anthracene	0.000
Benzene	0.117
Benzo(a)pyrene	0.000
Benzo(b)fluoranthene	0.000
Benzo(g,h,i)perylene	0.000
Benzo(k)fluoranthene	0.000
Chrysene	0.000
Dibenzo(a,h)anthracene	0.000
Dichlorobenzene	0.003
Ethylbenzene	0.003
	0.000
Fluoranthene	
Fluorene	0.000
Formaldehyde	5.538
Hexane	4.339
Indeno(1,2,3-cd)pyrene	0.000
Naphthalene	0.027
PAH	0.035
Phenanathrene	0.000
Propylene Oxide	0.219
Pyrene	0.000
Toluene	0.989
Xylenes	0.483
Arsenic	0.006
Beryllium	0.000
Cadmium	0.005
Chromiuim	0.009
Cobalt	0.000
Lead	0.007
Manganese	0.373
Mercury	0.001
Nickel	0.007
Selenium	0.007
Total HAPs ⁽²⁾	12.468

⁽¹⁾ Maximum emissions for each pollutant are the worst case emission of that pollutant for combustion turbine operation plus the emissions from the duct burner and auxiliary equipment.

⁽²⁾ Total HAP emissions are the maximum total HAP emissions from the combustion turbine (fuel oil firing) plus the total HAP emissions from the duct burner operation and auxiliary equipment.

Appendix B
Turbine Data

1/14/2006 FMPA			·				
Tressure Colest Energy Center Unit 1 Black & Vestch Project 138389,0030							
1x1 Emissions Estimates Case Number	1 1	2	3	4 1	5	6	7
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type CTG Load	Natural Gas	Distillate 100%	Natural Ges 100%	Oistillate 100%	Natural Gas	Oistillate	Natural Gas 100%
CTG trief Air Cooling	Evep. Cooler	Evap. Cooler	Off	Off	Evep. Cooler	Evap. Cooler	Evap. Cooler
CTG StemWater Injection Ambient Temperature, F	No 100	Water 100	No 26	Water 25	No. 73	Water 73	No 100
HRSG Duct Firing Fuel Sulfur Content (grains/100 standard cubic feet)	Fired 200	Fired 566,31	Fired 2.00	Fired 566.31	Fired 2.00	Fired 566.31	Unfired 2.00
Ambient Conditions							
Ambiert Temperature, F	100.0	100.0	28.0	28.0	73.0	73.0	100.0
Ambient Relative Humidity, %	48.4	48.4	100.0	100.0	81.5	81.5	48.4
Atmospheric Pressure, paia	14.690	14.690	14.590	14.690	14.690	14.690	14 590
Combustion Turbine Performance	ļ						
CTG Performance Reference	GTP	GTP	GTP	GTP	GTP	GTP	GTP
CTG Inlet Air Conditioning Effectiveness, % CTG Compressor Inlet Dry Butb Temperature, F	85.2 85.2	85.2	0 26.0	0 26.0	85 69.5	85 69.5	85.2 85.2
CTG Compr. triet Relative Humidity, %	89,7	89.7	100.0	100.0	97.0	97.0	89.7
Iniet Loss, in. H2O	40	4.0	4.0	4.0	4.0	4.0	4.0
Exhaust Loss, in, H2O	13.2	14.1	16.7	18.1	14.3	15.4	13.2
CTG Lord Level (percent of Base Load) Gross CTG Output, KW	100% 154,500	100% 163,400	100% 183,500	100%	100% 163,800	100% 173,200	100%
Gross CTG Heat Rate, BlukWh (LHV)	9,650	10,310	9,220	10,050	9,480	10,200	9,650
Gross CTG Heat Rate, BrunkWh (HHV)	10,705	10,980	10,228	10,704	10,516	10,863	10,705
CTG Heat Input, MBtuh (LHV) .CTG Heat Input, MBtuh (HHV)	1,490.9 1,653.9	1,684.7 1,794.2	1,691.9 1,878.8	1,919.6 2,044.4	1,552.8 1,722.5	1,768.8 1,881.5	1,490.9 1,653.9
	1,853.9				1,722.5		
CTG Water/Steam Injection Flow, 8th Injection Fluid/Fuel Ratio	0.0	109,030	0.0	143,570	0.0	122,910 1.3	0.0
CTG Exhaust Flow, Ib/h	3,357,000	3,483,000	3,834,000	4,004,000	3,506,000	3,651,000	3,357,000
CTG Exhaust Temperature, F	1,148	1,136	1,082	t,060	1,129	1,113	1,148
Combission Turbine Fuel Total CTG Fuel Flow, Ibrh	71,620	92,060	81,280	104,890	74,600	96,540	71,520
CTG Fuel Temperature, F	365	60	365	60	365	60	365
CTG Fuel LHV, Bluftb	20,816	18,300	20,816	18,300	20,816	18,300	20,816
CTG Fuel HHV, Blufts HHV/LHV Ratio	23,091 1.1093	19,490 1.0650	23,091 1.1093	19,490	23,091 1.1093	19,490 1.0650	23,091 1,1093
CTG Fuel Composition (Utimate Analysis by Weight)	_						
Ar	0.00%	0.00% 85.00%	0.00% 73.75%	0 00% 85.00%	0.00% 73.76%	0.00% 85.00%	0.00% 73.76%
H2 N2	24.01%	14.80%	24.01% 0.51%	14.80%	24.01% 0.61%	14.80% 0.20%	24.01%
02	1.61% 0.00657%	0.00%	1.61%	0.00%	1.61%	0.00%	1,619
S Total	100.00%	0.00150%	0.00857% 100.00%	0.00150%	0.00657% 100.00%	100.00%	0.006579
Fuel Sulfur Content (grains/100 standard cubic feet)	2.00	566.31	2.00	566.31	200	566.31	2.00
Combustion Turbine Exhaust							
CTG Exhaust Analysis (Yohana Basis Weg)	0.91%	0.87%	0.94%	0.89%	0.92%	0.88%	0.919
CO2 H2O	3.69%	5.24%	3.71% 7.65%	5.24% 11.49%	3.69%	5.26% 12.90%	3.699
N2	72.44%	69.45%	74.85%	71.18%	73.42%	70,10%	72.449
O2 SO2, (after SO2 oxidation)	12.25% 0.00010%	10.72% 0.00003%	12.86% 0.00010%	0.00003%	12.50% 0.00010%	10.87% 0.00003%	12.255 0.000105
SO3, (after SO2 coddation) Total	0.00002% 100.0%	0.00001%		0.00001%	0.00002%	0.00001%	0.000021
Molecular W1, Ib/mol	28,13	28,01	28.47	28.26	28.27	28.11	28.1
Specific Volume, N°3/lb Specific Volume, act/lb	40.43 13.49	40.18 13.54	37.99 13.33	37.61 13.43	39.65 13.42	39 38 13,50	40,4
Educati Ges Flow, actm Exhaust Ges Flow, actm	2,262,059 754,786	2,332,449 785,997	2,427,581 851,787	2,509,841 898,229	2,316,882 784,175	2,396,273 821,475	2,262,05 754,78
CTO NOt Entersions (Without Post Combustion Emissions Combrol)		/907/2018/2018/2018/2018				621,475 CARLES AND ACT OF 12 AND	
িটোল KCTII NOx Emissions (Without Post Combustion Emissions Control) ১৯ বেটাকেন্স কাল্যক্ষেত্ৰকাৰ নাজ্যক্ষিত আল একন্দ Additional Percent Margin included in mass based NOx Emissions below	04 04	0%	0%	9-12-2-19-20-20-20-20-20-20-20-20-20-20-20-20-20-	0%	0%	TO THE SECOND SE
NOx, pprivid (dry, 15% O2)	9.00	42.00	9.00	42.00	9.00	42.00	9.0
NOs, pprivd (dr) NOs, pornive (wet)	10.90 9.70	60.00	10,60	58.50 51.80	10.80	59.70 52.00	10.9
NOS, IDM as NO2 NOS, IDM as NO2 NOS, IDM as NO2	55.0 0.0369		62.0 0.0366	342.0 0.1782	57.0 0.0367	315.0 0.1783	55:
NOx, IDMBtu (HHV)	0.0333	0.1781	0.0330	0.1782	0.0387	0.1783	0.033
CTG CO Emissions (Without Post Combustion Emissions Control)		AND PRODUCTION OF THE	Entransista	hijakan 1965 (1967 1968)		100000000000000000000000000000000000000	*/_FJGBANNANAPA
Additional Percent Margin included in mass based CO Emissions below	04	0%					0
CO, pprivd (dry, 15% O2) CO, pprivd (dry)	7.40 9.00	14.00 20.00	7.60 9.00	14.40	7.50 9.00	14.10 20.00	7.4
CO, pprinter (wet) CO, bith	8 00 27.0	17.30	8.30 31.4	17.70	8.10 28.3		8.0
CO, to/MBtu (LHV)	0.0181 0.0163	0.0357	0 0185	0.0366	0.0162	0.0362	0.018
CO, IMASIL (HHV)		<u> </u>			0.0164		0.016
224 CTG 602 Emissions (After 802 Oxydiation, Without Post Combustion Emissions Control) 2022 (Additional Percent Margin included in bith 502 Emissions below	9045531 - 8564, 74554, 71 (7)	-(3) (3) (4) (4) (4) (4) (4) (4) (4) (4) (4) (4	0.09	STATE CALLS COME	0.0%	0.0%	0.0
Assumed \$02 oxidation rate in CTG, vol%	20.09	20.0%					20.0
SO2, pprived (dry, 15% O2) SO2, pprived (dry)	0.9083			0.2247 0.3130		0.2247 0.3194	0.900
SO2, ppmve (vet)	0.9839	0.2771	0.9894	0.2771	0.9861	0.2782	1,101 0,963
SO2, Ibh SO2, IbhBtu (LHV)	7.5216 0.0050	0.0013	8.5362 0.0050		0.0050	0.0013	7.521
SO2, IXMBtu (HHV)	0.0045	0.0012	0.0045	0.0012	0.0045	0.0012	0.004
							<u> </u>

U-14/2006 FMPA Treasure Coast Energy Center Unit 1							
Treasure Coast Energy Center Unit 1							
Black & Vestch Project 138859.0030							
1x1 Emissions Estimates							
Case Number	1	2	3	4	5	6	7
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type	Natural Gas 100%	Distillate 100%	Natural Gas	Distillate	Natural Ges 100%	Distillate 1	Natural Gas 100%
CTG Load CTG Inlet Air Cooking	Evap. Cooler	Evap. Cooler	100% Off	100% Off	Evap. Cooler	Evap. Cooler	Evap. Cooler
CTG Steam/Water Injection	No.	Water	No.	Water	No.	Water	No.
Ambient Temperature, F	100		26	26	73	73	100
HRSG Duct Firing	Fired		Fired	Fired	Fired	Fired	Unfired
Fuel Sulfur Content (grains/100 standard cubic feet)	2.00	566.31	2.00	566,31	2.00	566,31	2.00
Combustion Turbine Exhaust - continued							
	Tropic services	SANSON SEA PRIOR		244 4 7424/90398	Was can last amonator	***************************************	P74/24/P3/04/P3/
CTO UHC Emissions (Without Post Combustion Emissions Control)							- Trans Birthrought - Jours - Libertrane
Additional Percent Margin included in Ib/h UHC Emissions Below	0.0%	0.0%	0.0%	0.0%	0.0%	0.0%	0.0%
UHC, ppmwd (dry, 15% O2)	6.5	5.7	6.4	5.7	6.4	5.7	6.5
UHC, pprival (dry)	7.8	8.1	7.6	7.9	7.7	8.0	7.8
UHC, pprmw (wet)	7.0	7.0	7.0	7.0	7.0	7.0	7.0
UHC. Ib/h as CH4	13.4	14.0	15.1	16.0	140	15.0	13.4
UHC, Ib/MBtu as CH4 (LHV)	0.0090	0.0083	0.0089	0.0083	0.0090	0.0085	0.0090
UHC, RMBtu as CH4 (HHV)	0.0061	0.0078	0.0081	0.0078	0.0081	0.0080	0.0081
CTG VOC Britishous (Without Post Compustion Emissions Control)	CONTRACTOR CONTRACTOR	As the leavest president	SOLITON STATE	CRECAL VERNET	facilities and property of	ialimentament	AND LONDON STREET, STR
Additional percent margin included in Ib/h VOC emissions below	0%	0%	0%	0%	0%	0%	0%
VOC percentage of UHC	20%	50%	20%	50%	20%	50%	20%
VOC, ppmvd (dry, 15% O2)	1.3	2.8	1.3	2.8	1,3	2.8	1.3
VOC, ppmred (dry)	1.8	4.1	1.5	4.0	1,5	40	1.6
VOC, pprover (wet)	1.4	3.5	1.4	3.5	1.4	3.5	1,4
VOC, fb/h as CH4	2.7	7.0	3.0	8.0	2.8	7.5	2.7
VOC, fb/M8tu as CH4 (LHV)	0.0018	0.0042	0.0018	0.0042	0.0018	0.0042	0.0018
VOC, Ib/MBtu as CH4 (HHV)	0.0018	0.0039	0.0015	0.0039	0.0016	0.0040	0.0016
CTG PM10 Emissions (without the Effects of SCI Oxidation)		THE THE PROPERTY AND ADDRESS.	REAL COLUMN SERVICE	County and the second	VERTA CONTRACT	200000000000000000000000000000000000000	\$15.5:905K\$\$
Percent margin included in PM10 emissions below	0%	0%	0%	0%	0%	0%	
				_			
PM10 Emissions - Front Half Catch Only	 	- 170					
PM10, b/n	9.0	17.0	9.0	17.0	9.0	17.0	9.0
PM10, IDMBtu (LHV)	0.0060	0.0101	0.0053	0.0089	0.0058	0.0096	0.0060
PM10, lb/MBtu (HHV)	0,0054	0,0095	0.0048	0.0083	0.0052	0.0090	0.0054
PM10 Emissions - Front and Back Helf Catch				-			
PM10 Entraports - Front and suck read Cates	18.0	34.0	18.0	34.0	18.0	34.0	18.0
PM10, Ib/MBtu (LHV)	0.0121	0.0202	0.0106	0.0177	0.0118	0.0192	0.0121
PM10, IMMBtu (HHV)	0.0109	0.0189	0.0096	0.0166	0.0104	0.0181	0.0109
HRSG Duct Burners		<u> </u>					
-							
WRSG Duct Burners		(0) (100 / 6 (0) (0) (0)		AC ALWEST COM		21	
-	499.6	499.6	471,3	498.3	491.7	499.5	0.0
Duct Burner Flast (MBbuh (LHV) Duct Burner Hest Input, MBbuh (LHV) Duct Burner Hest Input, MBbuh (HHV)	499.6 554.2	499.6 554.2	471,3 522.8	498.3 552.8	491.7 545.4	499.5 554.2	0.0
Duct Burner Rest Input, MStuft (LHV)	499.6	499.6	471,3	498.3	491.7	499.5	0.0
Duct Burner Flast (MBbuh (LHV) Duct Burner Hest Input, MBbuh (LHV) Duct Burner Hest Input, MBbuh (HHV)	499.6 554.2	499.6 554.2	471,3 522.8	498.3 552.8	491.7 545.4	499.5 554.2	0.0
Duct Burner Feet Input, MBbuh (LHV) Duct Burner Heet Input, MBbuh (LHV) Total Duct Burner Feet Flow, boh	499.6 554.2 24,000	499.6 554.2 24.000	471.3 522.8 22,640	498.3 552.8 23,940	491.7 545.4 23,620	499.8 554.2 24,000	0.0 0.0 0.0
Duct Burner Fuel 1 (PU), MSbuft (LHV) Duct Burner Heet Input, MSbuft (LHV) Total Duct Burner Fuel Flow, Both Duct Burner Fuel Flow, Both	499.6 554.2 24,000	499.6 554.2 24,000	471.3 522.8 22,640 20,816	496.3 552.8 23,940 20,816	491.7 545.4 23,620 20,816	499.5 554.2 24,000 20,815	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
Duct Burner Feet Input, MBbuh (LHV) Duct Burner Heet Input, MBbuh (LHV) Total Duct Burner Feet Flow, boh	499.6 554.2 24,000	499.6 554.2 24.000	471.3 522.8 22,640	498.3 552.8 23,940	491.7 545.4 23,620	499.8 554.2 24,000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
Duct Burner Fues (** 2008) Duct Burner Heest Input, MSbuft (LHV) Duct Burner Heest Input, MSbuft (HHV) Total Duct Burner Fuel Flow, both Duct Burner Fuel LHV, Bbuftb Duct Burner Fuel LHV, Bbuftb	499.6 554.2 24,000	499.6 554.2 24,000	471.3 522.8 22,640 20,816	496.3 552.8 23,940 20,816	491.7 545.4 23,620 20,816	499.5 554.2 24,000 20,815	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
Duct Burner Fuel Plus, MBbuft (LHV) Duct Burner Heet Input, MBbuft (LHV) Total Duct Burner Fuel Flow, Bdh Duct Burner Fuel LHV, Bbufb Duct Burner Fuel HHV, Bbufb Duct Burner Fuel HHV, Bbufb Duct Burner Fuel HHV, Bbufb	499.6 554.2 24,000 20,816 23,091	499.6 554.2 24,000 20,816 23,091	471,3 522.8 22,840 20,816 23,091	498.3 552.8 23,940 20,816 23,091	491.7 545.4 23,620 20,816 23,091	499.5 554.2 24,000 20,816 23,091	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
Duct Burner Fuel ("July Mittuh" (LHV) Duct Burner Heet Input, Mittuh" (LHV) Duct Burner Heet Flow, Both Duct Burner Fuel Flow, Both Duct Burner Fuel HHV, Blutb Duct Burner Fuel HHV, Blutb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar	499.6 554.2 24,000 20,816 23,091	499.6 554.2 24,000 20,816 23,091	471.3 522.8 22,840 20,816 23,091	498.3 552.8 23,940 20,816 23,091	491.7 545.4 23,820 20,816 23,091	499.5 554.2 24,000 20,815 23,091	20,819 20,819 20,000
Duct Burner Fuel ("Duty, MBbuft (LHV) Duct Burner Heet Input, MBbuft (LHV) Total Duct Burner Fuel Flow, bbft Duct Burner Fuel LHV, Bbuftb Duct Burner Fuel LHV, Bbuftb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C	499.6 554.2 24,000 20,816 23,091	499.6 554.2 24,000 20,816 23,091 0,00% 73,78%	471.3 522.8 22,840 20,816 23,091	498.3 552.8 23,940 20,816 23,091	491.7 545.4 23,620 20,816 23,091 0.00%, 73,76%,	499.5 554.2 24,000 20,816 23,091 0.00% 73,78%	0.0 0.0 0.0 20.816 23.091
Duct Burner Fuel ("J. M.Bhuft (J.HY) Duct Burner Heet Input, MBhuft (J.HY) Duct Burner Heet Input, MBhuft (HHY) Total Duct Burner Fuel Flow, Brh Duct Burner Fuel HHY, Bhuftb Duct Burner Fuel HHY, Bhuftb Duct Burner Fuel HHY, Bhuftb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C C H2	499.6 554.2 24,000 20,816 23,091 0,00% 73,76% 24,01%	499.8 554.2 24.000 20,816 23,091 0.00% 73,76% 24.01%	471.3 522.8 22,840 20,816 23,091 0,00% 73,76% 24,01%	498.3 592.8 23.940 20.816 23.091 0.00% 73.76% 24.01%	491.7 545.4 23,620 20,816 23,091 0,00%, 73,75%, 24,01%	499.5 554.2 24,000 20,816 23,091 0,00% 73,79% 24,01%	0.00 0.00 0.00 20.816 23.991 0.009 73.791
Duct Burner Fuel ("All Burner Fuel ("All Burner Fuel Flow, MSbuth (LHV) Duct Burner Heat Input, MSbuth (LHV) Total Duct Burner Fuel Flow, both Duct Burner Fuel LHV, Bbutb Duct Burner Fuel LHV, Bbutb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C HZ	499.6 554.2 24,000 20,816 23,091	499.6 554.2 24,000 20,816 23,091 0,00% 73,76% 24,01% 0,61%	471.3 522.8 22,840 20,816 23,031 0,00% 73,76% 24,01%	498.3 592.8 23.940 20.816 23.091 0.00% 73.76% 24.01%	491.7 545.4 22,620 20,816 23,091 0,00%, 73,76%, 24,01%	499.5 554.2 24,000 20,815 23,091 0,00% 73,76% 24,01% 0,61%	0.0 0.0 0 20,816 23,091 73,767 24,011 0.811
Duct Burner Fuel ("J. M.Bhuft (J.HY) Duct Burner Heet Input, MBhuft (J.HY) Duct Burner Heet Input, MBhuft (HHY) Total Duct Burner Fuel Flow, Brh Duct Burner Fuel HHY, Bhuftb Duct Burner Fuel HHY, Bhuftb Duct Burner Fuel HHY, Bhuftb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C C H2	490.6 554.2 24,000 20,816 23,091 0 00% 73,76% 24,011 0 61%	499.6 554.2 24,000 20,816 23,091 0,00% 73,78% 24,01% 0,61% 1,61%	471.3 522.8 22,840 20,816 23,091 0,00% 73,76% 24,01%	498.3 592.8 23.940 20.816 23.091 0.00% 73.76% 24.01%	491.7 545.4 23,620 20,816 23,091 0,00%, 73,75%, 24,01%	499.5 554.2 24,000 20,816 23,091 0,00% 73,79% 24,01%	0.00 0.00 0.00 20.818 23.091 0.009 73.787 24.017 0.817
Duct Burner Flads (**) 2008/2008/2009 Duct Burner Healt Input, Mithuth (LHV) Duct Burner Healt Input, Mithuth (HHV) Total Duct Burner Flad Flow, bith Duct Burner Flad HHV, Bluttlb Let Burner Flad Composition (Ultimate Analysis by Weight) Ar C H2 H2 H2 H2 H2 H2 H2 H2	499.6 554.2 24,000 20,816 23,091 0.000 73,76% 24,01% 0.61%	499.6 554.2 24,000 20,616 23,091 0,00% 73,78% 24,01% 0,01% 1,61% 0,0057%	471.3 522.8 22.840 20.816 23.091 0.00% 73.76% 24.01% 0.61%	498.3 592.8 23.940 20.816 23.091 0.00% 73.76% 24.01% 0.61%	491.7 545.4 23,620 20,816 23,091 0,00%, 73,76%, 24,01%, 0,61%,	499.5 554.2 24,000 20,816 23,091 0,00% 73,76% 24,01% 0,61%	0.0 0.0 0.0 0.0 20.818 23.091 0.0097 24.011 0.611 1.0111 0.00577
Duct Burner Fues (** ** ** ** ** ** ** ** ** ** ** ** **	499.6 554.2 24,000 20,816 23,091 0,00% 7.3,70% 24,01% 0,61% 1,61% 0,0057%	499.6 \$54.2 24.000 20,816 23,091 0.005 73,76% 24.01% 0.01% 1.61% 0.00557%	471.3 522.6 22,640 20,816 23,091 0,00% 73,78% 24,01% 0,61% 0,00957%	498.3 552.8 23.940 20.816 23.091 0.00% 73.78% 24.01% 0.61% 1.61%	491.7 545.4 22,620 20,816 23,091 0,00%, 73,76%, 24,01%, 0,61%, 1,61%,	499.5 554.2 24.000 20.915 23.091 0.00% 73.78% 24.01% 0.61% 1.61% 0.00657%	0.0 0.0 0.0 0.0 0.0 0.0 0.0 73.79 24.01 1.01 1.01 0.00557
Duct Burner Fuel ("Duty, MBUsh (LHV) Duct Burner Heet Input, MBUsh (LHV) Total Duct Burner Fuel Flow, bith Duct Burner Fuel LHV, Btutb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 R2 Q2 S Total Fuel Suffue Content (grains/100 standard cubic feet)	499.8 554.2 24,000 20,816 23,091 0.005 72,75% 24,01% 0.61% 1.81% 0.00557% 1.00007%	499.6 \$54.2 24.000 20,816 23,091 0.00% \$73.75% 24.01% 0.01% 1.61% 0.00657% 100.0% 2.00	471.3 \$22.6 22.640 20.816 23.091 0.0095 73.76% 24.01% 0.01% 1.61% 0.00657% 1.00.0%	496.3 582.8 23.940 20.916 23.001 0.0005 73.765 24.015 0.0057% 1.015 0.00057%	491.7 545.4 22,650 20,816 23,001 0,00% 73,76% 24,01% 1,61% 0,00657% 100,0% 2,00	499.5 554.2 24,000 20,815 23,091 0,00% 73,75% 24,01% 0,61% 1,15% 1,00% 1	0.0 0.0 0.0 0.0 0.0 0.0 0.0 73.79 24.01 1.01 1.01 0.00557
Duct Burner Fuel Plant, MBbuft (LHV) Duct Burner Heet Input, MBbuft (LHV) Total Duct Burner Fuel Flow, bbft Duct Burner Fuel LHV, Bbufb Duct Burner Fuel LHV, Bbufb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 N2 O2 S Total	499.8 554.2 24,000 20,816 23,091 0.005 72,75% 24,01% 0.61% 1.81% 0.00557% 1.00007%	499.6 \$54.2 24.000 20,816 23,091 0.005 73,76% 24.01% 0.01% 1.61% 0.00557%	471.3 S22.6 22.640 20.816 23.091 0.0095 73.76% 24.01% 0.015% 1.61%	496.3 582.8 23,840 20,816 23,001 0,005 73,76% 24,01% 0,015% 1,11% 0,00657%	491.7 545.4 22,650 20,816 23,001 0,00% 73,76% 24,01% 0,0657% 1,01%	499.5 554.2 24,000 20,816 23,091 0,00% 73,76% 24,01% 0,61% 1,161% 0,00657% 1,000%	20.816 23.091 23.091 24.011 24.011 1.611 0.005577
Duct Burner Past "Allament Duct Burner Heat Input, MBbuth (LHV) Duct Burner Heat Input, MBbuth (HHV) Total Duct Burner Fuel Flow, both Duct Burner Fuel LHV, Bbutb Duct Burner Fuel LHV, Bbutb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 N2 02 S Total Fuel Suffer Content (grains/100 standard cubic feet) Duct Burner Fuel Suffer Content (grains/100 standard cubic feet) Duct Burner Fuel B	499.6 554.2 24,000 20,816 23,091 0,00% 73,75% 24,01% 0,01% 1,61% 1,000 10,000 2,000 10,000	499.6 554.2 24,000 20,616 23,091 0,00% 73,78% 24,01% 0,01% 1,61% 0,0057% 100.0% 2,000	471.3 522.6 22,640 20,816 23,091 0,00% 73,787% 24,01% 0,61% 1,61% 0,0057% 100.0%	498.3 552.8 23,940 20,816 23,091 0,00% 73,78% 24,01% 0,61% 1,61% 1,00% 2,000 2	491.7 545.4 22,620 20,816 23,091 0,00%, 73,76%, 24,01%, 0,01%, 1,61%, 1,00%, 2,	499.5 554.2 24,000 20,816 23,091 0,00% 73,78% 24,01% 0,0557% 100,00% 2,00	20,818 23,091 23,091 24,011 24,011 1611 0,008577 10000
Duct Burner Fuel (Publ. MBbuft (LHY) Duct Burner Heet Input, MBbuft (LHY) Total Duct Burner Fuel Flow, Brb Duct Burner Fuel Flow, Brb Duct Burner Fuel Flow, Brb Duct Burner Fuel HHY, Btufb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 N2 Q2 S Total Fuel Suffur Content (grains/100 standard cubic feet) Ar Duct Burner Figitations Duct Burner HOS, BMBB (HHY) Duct Burner HOS, BMBB (HHY)	499.6 554.2 24,000 20,816 23,091 0.005 73,76% 24,01% 0.61% 1.81% 0.00557% 100.0% 0.000	499.6 554.2 24.000 20,816 23,991 0.00% 73,796 24.01% 0.01% 1.61% 1.00% 0.005 0.000	471.3 \$22.6 22.640 20.816 23.091 0.00% 73.76% 24.01% 0.00857% 10.0% 0.00857%	496.3 562.8 23,940 20,916 23,091 0,005 73,795 24,01% 0,018 1,01% 1,01% 0,005 0,000 0,000	491.7 5-45.4 23,000 23,001 0,005,73,793,703,703,703,703,703,703,703,703,703,70	499.5 554.2 24,000 20,815 23,091 0,00% 73,75% 24,01% 0,61% 1,15% 1,00% 1	20,818 23,091 0,000 73,787 24,011 0,00577 1000 1000 2,000 1000 1000 1000 1000 100
Duct Burner Fuel Plans, MSbuft (LHV) Duct Burner Hest Input, MSbuft (LHV) Total Duct Burner Hest Input, MSbuft (LHV) Total Duct Burner Fuel LHV, Bbuft Duct Burner Fuel LHV, Bbuft Duct Burner Fuel LHV, Bbuft Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 W2 02 S Total Fuel Suffer Content (grains/100 standard cubic feet) C Burt Burner RU, Bhuft Duct Burner RU, BhuftBu (HHV) Duct Burner CO, BhuftBu (HHV)	499.6 564.2 24,000 20,816 23,091 0,00% 73,70% 24,01% 0,61% 1,161% 0,00579 100,00% 2,000 0,040 0,040	499.6 554.2 24,000 20,816. 23,091 0,00% 73,79% 24,01% 0,61% 1,01% 1,00% 1,0	471.3 522.6 22,640 20,816 23,091 0,00% 7.3 76% 24,01% 0,00857% 10,00% 2,000 0,000 0,000	498.3 552.8 23,940 20,816 23,091 0,00% 73,78% 24,01% 0,61% 1,61% 1,00% 2,000 2	491.7 545.4 22,620 20,816 23,091 0,00%, 73,76%, 24,01%, 0,01%, 1,61%, 1,00%, 2,	499.5 554.2 24,000 20,816 23,091 0,00% 73,78% 24,01% 0,0557% 100,00% 2,00	0.0 0.0 0.0 0.0 0.0 0.0 73.797 74.071 0.0 1.0 1.0 1.0 0.0 0.0 0.0 0.0 0.0 0.
Duct Burner Flads (** 30000000000000000000000000000000000	499.8 554.2 24,000 20,816 23,091 0.005 7.7 75% 24,018 0.61% 1.81% 0.00557% 1.000,000 0.000 0.000 0.000	499.6 554.2 24.000 20,816 23,091 0.0005 73,76% 24.01% 0.01% 1.61% 0.0005 0.000 0.000 0.000	471.3 \$22.8 22.840 20.816 23.091 0.005 73.76% 24.01% 0.0057% 1.61% 0.0067% 0.000 0.000 0.000 0.000 0.000	496.3 582.8 23,840 20,816 23,001 0,005 73,76% 24,01% 0,005 1,01% 0,005 0,000 0,000 0,000 0,000	491.7 545.4 22,870 20,816 23,091 0.005,73,76% 24,01% 0.00557% 1.61% 0.00567% 0.000 0.000 0.000	499.5 554.2 24,000 20,816 23,091 0,00% 73,798 24,01% 0,01% 1,61% 0,00657% 100,0% 0,000 0,000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
Duct Burner Host Input, MBbuh (LHV) Duct Burner Hest Input, MBbuh (LHV) Total Duct Burner Hest Flow, Bbh Duct Burner Fuel LHV, Bbulb Duct Burner Fuel LHV, Bbulb Duct Burner Fuel HHV, Bbulb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 N2 O2 S Total Fuel Suffur Content (grains/100 standard oubic feet) Duct Burner HOS, BMBbu (HHV) Duct Burner HOC, BMBbu (HHV) Duct Burner HOC, BMBbu (HHV) Duct Burner HOC, BMBbu (HHV) Duct Burner UCC (B BCH), BMBbu (HHV) Duct Burner WOC (BS CH4), BMBbu (HHV)	499.6 564.2 24,000 20,816 23,091 0,00% 73,75% 10,00	490.6 554.2 24.000 20.816 23.091 0.00% 73.78% 24.01% 0.01% 1.01% 1.03% 0.00857% 100.0% 0.000 0.000 0.000 0.000	471.3 522.6 22.640 20.816 23.091 0.00% 73.78% 24.01% 0.0057% 100.00% 0.000 0.000 0.000	498.3 582.8 23.840 20.816 23.091 0.00% 73.76% 24.01% 0.00% 1.61% 0.00% 0.0000 0.000 0.00	491.7 545.4 23,870 20,818 23,091 0,00% 73,76% 24,01% 0,01% 1,11% 0,00857% 100,07% 2,00 0,000	499.5 554.2 24,000 20,815 23,091 0,00% 73,76% 24,01% 0,61% 0,006 100,00% 2,000 0,000 0,000 0,000	20.818 23.091 23.091 23.091 24.019 24.019 0.005577 100.09 2.0
Duct Burner Flads (** 30000000000000000000000000000000000	499.8 554.2 24,000 20,816 23,091 0.005 7.7 75% 24,018 0.61% 1.81% 0.00557% 1.000,000 0.000 0.000 0.000	490.6 554.2 24.000 20.816 23.091 0.00% 73.78% 24.01% 0.01% 1.01% 1.03% 0.00857% 100.0% 0.000 0.000 0.000 0.000	471.3 \$22.8 22.840 20.816 23.091 0.005 73.76% 24.01% 0.0057% 1.61% 0.0067% 0.000 0.000 0.000 0.000 0.000	496.3 582.8 23,840 20,816 23,001 0,005 73,76% 24,01% 0,005 1,01% 0,005 0,000 0,000 0,000 0,000	491.7 545.4 22,870 20,816 23,091 0.005,73,76% 24,01% 0.00557% 1.61% 0.00567% 0.000 0.000 0.000	499.6 554.2 24,000 20,816 23,091 0,0006 73,76% 1,01% 0,0557% 1,01% 0,00667% 1,0006 0,000 0,000	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0
Duct Burner Host Input, MBbuh (LHV) Duct Burner Hest Input, MBbuh (LHV) Total Duct Burner Hest Flow, Bbh Duct Burner Fuel LHV, Bbulb Duct Burner Fuel LHV, Bbulb Duct Burner Fuel HHV, Bbulb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 N2 O2 S Total Fuel Suffur Content (grains/100 standard oubic feet) Duct Burner HOS, BMBbu (HHV) Duct Burner HOC, BMBbu (HHV) Duct Burner HOC, BMBbu (HHV) Duct Burner HOC, BMBbu (HHV) Duct Burner UCC (B BCH), BMBbu (HHV) Duct Burner WOC (BS CH4), BMBbu (HHV)	499.8 554.2 20,816 23,091 0,00% 73,70% 24,011 0,016 1,017 0,00% 1,	499.6 554.2 24.000 20.816 23.091 0.00% 73.78% 24.01% 0.01% 10.00% 100.00% 0.000 0.000 0.000 0.000 0.000 0.000	471.3 522.6 22.640 20.816 23.091 0.00% 73.78% 24.01% 0.01% 10.0057% 100.005 0.000 0.000 0.000 0.000	498.3 582.8 23,940 20,916 23,001 0,005 73,765 24,01% 0,005 1,01% 0,005 0,000 0,00	491.7 \$45.4 23,870 20,818 23,001 0,005, 73,778, 0,018, 1,018, 0,005, 2,00 0,000 0	499.5 554.2 24,000 20,815 23,091 0,00% 73,78% 24,01% 0,01% 1,01% 1,01% 1,00% 2,00 0,00% 0,00% 0,00% 0,00%	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0
Duct Burner Flast Input, MSbuft (LHV) Duct Burner Heat Input, MSbuft (LHV) Total Duct Burner Flast Flow, bth Duct Burner Flast Flow, bth Duct Burner Flast HrV, Bhuftb Duct Burner Flast HrV, Bhuftb Duct Burner Flast HrV, Bhuftb Duct Burner Flast Composition (Ultimate Analysis by Weight) Ar C H2 N2 O2 S Total Flust Suffur Content (grained 100 standard cubic feet) Duct Burner Hot, BhuftBlu (HHV) Duct Burner HOt, BouftBlu (HHV) Duct Burner HOt, BhuftBlu (HHV) Duct Burner HOt, BouftBlu (HHV) Duct Burner HOt, BhuftBlu (HHV) Duct Burner HOt, BouftBlu (HHV) Duct Burner FMH, BuftBlu (HHV) (front half catch only) Duct Burner FMH, BuftBlu (HHV) (front half catch only) Duct Burner FMH, BuftBlu (HHV) (front half catch only) Assumed SO2 oddation rate in Duct Burner, voffs	499.8 554.2 24,000 20,816 23,091 0,005 73,75% 24,0115 0,015% 1,81% 0,00577 100,0% 2,00 0,040 0,0	499.6 554.2 24,000 20,816 23,091 0,00% 73,78% 24,01% 0,01% 1,01% 1,00% 2,00 0,000	471.3 522.6 22,640 20,816 23,091 0,00% 7.3 79% 24,01% 0,01% 1,01% 1,00% 2,000 0,040 0,040 0,040 0,000 0 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0 0	496.1 582.8 23.940 20.916 23.091 0.005 73.765 24.015 0.005577 100.05 0.0050 0.005	491.7 545.4 22.670 20.816 23.001 0.00% 73.76% 24.01% 0.00657% 100.0% 0.006 0.000 0.000 0.000 0.000 0.000	499.5 554.2 24,000 20,816 23,091 0,00% 73,76% 24,01% 0,61% 1,01% 1,00% 2,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000	0.00 0.00 0.00 0.00 0.00 73.78 24.01 0.05 1.01 1.01 1.00 0.00 0.00 0.00 0
Duct Burner Flats (**DMBSUM* (LHV) Duct Burner Heat Input, MBSUM* (LHV) Total Burner Flats (**DMBSUM* (HHV) Total Burner Flats (**DMBSUM* (HHV) Duct Burner Flats (**DMBSUM* (HHV) Duct Burner Flats (**DMBSUM* (HHV) Ar C H2 N2 Q2 S Total Fluts Suffur Content (grains/100 standard cubic faet) Are Suffur Content (grains/100 standard cubic faet) Duct Burner Flats (**DMBSU* (HHV) Duct Burner WO, BN/BSU* (HHV) Duct Burner	499.6 554.2 24,000 20,816 23,091 0,00% 73,75% 24,01% 0,61% 1,61% 0,0057% 0,000	499.6 \$54.2 24.000 20,816 23,091 0.00% 73,79% 24.01% 0.01% 100.0% 100.0% 0.000	471.3 522.8 22.840 20.816 23.091 0.00% 73.78% 24.01% 0.00857% 100.0% 0.000	496.3 552.8 23,940 20,916 23,091 0,005 73,759 24,01% 0,016 10,0% 0,000 0	491.7 5-45.4 23,001 23,001 0.00%, 73,70%, 0.01%, 0.00%, 1.01%, 0.00857%, 0.000, 0.000	499.5 554.2 24,000 20,816 23,091 0,00% 73,79% 0,01% 0,00% 1,01% 0,00% 0,	20,811 23,09 0.00 73,76 24,01 0.085 1,00 0.00 0.00 0.00 0.00 0.00 0.00 0.00
Duct Burner Flast Input, MSbuft (LHV) Duct Burner Heat Input, MSbuft (LHV) Total Duct Burner Flast Flow, bth Duct Burner Flast Flow, bth Duct Burner Flast HrV, Bhuftb Duct Burner Flast HrV, Bhuftb Duct Burner Flast HrV, Bhuftb Duct Burner Flast Composition (Ultimate Analysis by Weight) Ar C H2 N2 O2 S Total Flust Suffur Content (grained 100 standard cubic feet) Duct Burner Hot, BhuftBlu (HHV) Duct Burner HOt, BouftBlu (HHV) Duct Burner HOt, BhuftBlu (HHV) Duct Burner HOt, BouftBlu (HHV) Duct Burner HOt, BhuftBlu (HHV) Duct Burner HOt, BouftBlu (HHV) Duct Burner FMH, BuftBlu (HHV) (front half catch only) Duct Burner FMH, BuftBlu (HHV) (front half catch only) Duct Burner FMH, BuftBlu (HHV) (front half catch only) Assumed SO2 oddation rate in Duct Burner, voffs	499.8 554.2 24,000 20,816 23,091 0,005 73,75% 24,0115 0,015% 1,81% 0,00577 100,0% 2,00 0,040 0,0	499.6 554.2 24,000 20,816 23,091 0,00% 73,78% 24,01% 0,01% 1,01% 1,00% 2,00 0,000	471.3 522.6 22,640 20,816 23,091 0,00% 7.3 79% 24,01% 0,01% 1,01% 1,00% 2,000 0,040 0,040 0,040 0,000 0 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0 0	496.1 582.8 23.940 20.916 23.091 0.005 73.765 24.015 0.005577 100.05 0.0050 0.005	491.7 545.4 22.670 20.816 23.001 0.00% 73.76% 24.01% 0.00657% 100.0% 0.006 0.000 0.000 0.000 0.000 0.000	499.5 554.2 24,000 20,816 23,091 0,00% 73,76% 24,01% 0,61% 1,01% 1,00% 2,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000	20,811 23,09 0.00 73,76 24,01 0.085 1,00 0.00 0.00 0.00 0.00 0.00 0.00 0.00
Duct Burner Heals (1904, MBbuth (LHV) Duct Burner Heals Input, MBbuth (LHV) Total Duct Burner Heal Flow, Buth Duct Burner Heal Flow, Buth Duct Burner Fuel HerV, Bhuth Duct Burner Fuel HerV, Bhuth Duct Burner Fuel HerV, Bhuth Duct Burner Fuel HerV, Bhuth Ar C H2 N2 O2 S Tratal Fuel Suffur Content (grains/100 standard cubic feet) Fuel Suffur Content (grains/100 standard cubic feet) Duct Burner HOS, BhitBbu (HHV) Duct Burner HOS, BhitBbu (HHV) Duct Burner HOS, BhitBbu (HHV) Duct Burner WOC (so CHM), BhitBbu (HHV) Duct Burner PMOL (so CHM) bhitBbu (HHV) Duct Burner PMOL (so MHBbu (HHV)) Total SOO3, Bhit from Duct Burner Fuel only (after SO2 coddation) Total SOO3, Bhit from Duct Burner Fuel only (after SO2 coddation)	499.6 554.2 24,000 20,816 23,091 0,000 773,75% 24,01% 0,61% 1,61% 1,000 0,000	499.6 \$54.2 24.000 20,816 23,091 0.00% 73,78/% 24.01% 0.01% 1.01% 0.005 0.000 0	471.3 522.8 22.840 20.816 23.091 0.005 73.765 24.01% 0.00857% 10.0% 0.0060 0.0000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.0000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.0000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.0000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.0000 0.	496.3 582.8 23,940 20,916 23,091 0,005 73,795 24,01% 0,016 101,005 0,000	491.7 5-45.4 22,000 23,000 0.00%, 73,79%, 24,01%, 0.0057%, 100.0%, 0.000	499.5 554.2 24,000 20,816 23,091 0,00% 73,79% 1,61% 0,06857% 100,0% 0,000 0,00	20,811 23,09° 0,00° 73,76° 24,01° 0,05° 100,0° 0,00° 0
Duct Burner Hest Input, MBbuth (LHV) Duct Burner Hest Input, MBbuth (LHV) Total Duct Burner Hest Input, MBbuth (LHV) Total Duct Burner Fuel LHV, Bbutb Duct Burner Fuel HHV, Bbutb Duct Burner Fuel HHV, Bbutb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 N2 O2 S Total Fuel Suffur Content (grains/100 standard cubic feet) Duct Burner Bysistions Duct Burner Hysistions Du	499.6 564.2 24,000 20,816 23,091 0,00% 73,70% 24,01% 0,61% 1,61% 0,0057% 100,0% 0,000 0,00	490.6 554.2 24.000 20.816 23.091 0.00% 73.78% 10.0% 1.61% 0.00857% 10.0% 0.000 0.000 0.040 0.000 0.000 0.040 0.000	471.3 522.6 22.640 20.816 23.091 0.005, 73.709, 24.01% 0.00557% 100.0% 2.00 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 10.000 0.000 10.000 0.000	498.3 SS2.8 23.940 20.816 23.091 0.00% 73.78% 24.01% 0.01% 1.61% 0.00% 2.00 0.000	491.7 545.4 23,820 20,818 23,091 0,005, 73,76%, 0,61%, 1,61%, 0,00857%, 100,07%, 2,000 0	499.5 554.2 24.000 20.015 23.091 23.091 24.000 25.091 24.000 25.091 25.09	0.00 0.00
Duct Burner Heal (1) 2008/2009 (LHV) Duct Burner Heal Input, MBbuth (LHV) Duct Burner Heal Input, MBbuth (LHV) Total Duct Burner Fuel Flow, bith Duct Burner Fuel HVV, Bbutlb Ar C H2 N2 O2 S Total Fuel Suffur Content (grains/100 standard cubic feet) Duct Burner NO, Bh/Bbut (HVV) Duct Burner NO, Bh/Bbut (HVV) Duct Burner NO, Bh/Bbut (HVV) Duct Burner VOC (Bh/Bbut (HVV) Duct Burner VOC (Bh/Bbut (HVV) Duct Burner VOC (Bh/Bbut (HVV) Duct Burner PMIO, Bh/Bbut (HVV) (front heaf catch only) Duct Burner PMIO, Bh/Bbut (HVV) (front heaf catch only) Duct Burner PMIO, Bh/Bbut (HVV) (front heaf catch only) Total SOO, Bh/Bron Duct Burner Fuel only (after SO2 caddation) DB NOx, Bh DB NOx, Bh DB NOx, Bh DB ROx, Bh	499.8 554.2 20,816 23,091 0.005 7.7 75% 24,018 0.61% 1.81% 0.00557% 1.00,005 0.0000 0.000 0.000 0.000 0.000	499.6 \$54.2 24.000 20,816 23,091 0.005 73.76% 24.01% 0.61% 1.61% 0.005 0.000 0.00	471.3 522.8 22.840 22.840 2.091 2.001 2.0095 2.100 2.0095 2.4.01% 0.0085 2.00 0.000	496.3 582.8 23,940 20,916 23,001 0,005 73,76% 24,01% 0,006 1,01% 0,006 0,00	491.7 545.4 23,600 20,816 23,001 0.005, 73,76%, 24,01%, 0.065, 1.61%, 0.0065, 0.000	499.6 554.2 24,000 20,816 23,091 0,000 0,000 1,101% 0,00567% 1,01% 0,00667% 0,000 0,	0.000 0.000 0.000 7.3.78*2.24.01 0.0000 0.000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0
Duct Burner Flast (1904, MBbuh (LHV) Duct Burner Hest Input, MBbuh (LHV) Total Duct Burner Flast Flow, Both Duct Burner Flast Composition (Ulfimate Analysis by Weight) Ar C H2 N2 O2 S Total Flast Suffur Content (grainat/100 standard cubic feet) Duct Burner ROs, BMBbu (HHV) Duct Burner ROs, BMBbu (HHV) Duct Burner OO, BMBbu (HHV) Duct Burner UNC (ise CH4), BMBbu (HHV) Duct Burner PMO, BMBbu (HHV) Total SO2, BMBbu (HHV) Duct Burner PMO, BMBbu (HHV) (front half cetich only) Duct Burner PMO, BMBbu (HHV) (front half cetich only) Duct Burner PMO, BMBbu (HHV) (front half cetich only) Duct Burner PMO, BMBbu (HHV) (front half cetich only) Duct Burner SMO, BMBbu (HHV) (front half cetich only) Duct Burner SMO, BMBbu (HHV) (front half cetich only) Duct Burner SMO, BMBbu (HHV) (front half cetich only) Duct Burner SMO, BMBbu (HV) (front half cetich only) Duct Burner SMO, BMBbu (HV) (front half cetich only) Duct Burner SMO, BMBbu (HV) (front half cetich only) Duct Burner SMO, BMBbu (HV) (front half cetich only) Duct Burner SMO, BMBbu (HV) Duct Burne	499.8 554.2 20,816 23,091 0,00% 73,70% 0,51% 0,10% 10,00% 10,00% 0,000 0	499.6 554.2 24.000 20,816 23,091 0.00% 73.70% 24.01% 0.01% 10.00% 10.00% 0.000	471.3 522.8 22.840 20.816 23.091 0.00% 73.78% 24.01% 0.0057% 100.0	496.3 55.2 8 23.940 20.816 23.901 0.00% 73.73/76% 24.01% 0.00%77 100.0% 0.000	491.7 545.4 23,870 23,870 23,870 0.00%, 73,77%, 0.61%, 1.61%, 0.00857%, 100.0%, 2.00 0.000	499.5 554.2 24,000 20,815 23,091 0,00% 73,79% 0,05% 1,01% 0,06% 1,00% 0,086 0,	20,811 23,091 0,000 73,379 24,011 0,000 1,000 0
Duct Burner Flast Input, MSbuft (LHV) Duct Burner Hest Input, MSbuft (LHV) Total Duct Burner Hest Input, MSbuft (LHV) Total Duct Burner Fuel LHV, Bbufb Duct Burner Fuel LHV, Bbufb Duct Burner Fuel LHV, Bbufb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 N7 O2 S Total Feet Suffer Content (grains/100 standard cubic feet) S Duct Burner MO, BMBbb (HHV) Duct Burner LNG (see HH), BMBbb (HHV) Duct Burner MO, BMBbb (HHV) Duct Burner MO, BMBbb (HHV) Duct Burner MO, BMBbb (HHV) Duct Burner MO (see CHH), BMBbb (HHV) Duct Burner MO (see CHH), BMBbb (HHV) Duct Burner MO (see CHH) for fair and seek half catch) Assumed SC2 oddation rate in Duct Burner, woffs Total SO2, Bnh from Duct Burner Fuel only (after SO2 oddation) Total SO3, Bnh from Duct Burner Fuel only (after SO2 oddation) DB NOs, Bnh DB CO, Bnh DB UHC (see CHH), Bnh	499.8 554.2 24,000 20,816 23,091 0,005 73,75% 24,01% 0,15% 0	499.6 554.2 24.000 20,616 23,091 0,0005 73.75% 24.01% 0,01% 1,01% 0,0005 0,040 0,000 0,040 0,010 0,024 10,0% 10,0% 2,836 0,334 44.33 22,20 33,30	471.3 \$22.8 22.840 2.091 0.0095 73.78% 24.01% 0.00557% 1.01% 0.00057% 1.00% 0.0000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0	496.3 582.8 23.940 20.916 23.001 0.00557 1.015 0.00557 1.00.05 0.006	491.7 545.4 22.650 20.816 23.001 0.00% 73.76% 24.01% 0.0057% 1.01% 0.00607% 0.0000 0.0000 0.0000 0.0000 0.0000 0.0	499.6 554.2 24.000 20.816 23.091 0.00% 73.78% 24.01% 0.01% 0.00% 1.00% 0.000 0	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0
Duct Burner Heat Input, MBbuth (LHV) Duct Burner Heat Input, MBbuth (LHV) Total Duct Burner Fuel Flow, Bbth Duct Burner Fuel Flow, Bbth Duct Burner Fuel Flow, Bbth Duct Burner Fuel HHV, Bbutb Duct Burner Fuel HHV, Bbutb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 N2 O2 S Total Fuel Suffur Content (grains/100 standard cubic feet) Fuel Suffur Content (grains/100 standard cubic feet) Duct Burner Pote Bbuth (HHV) Duct Burner HOS, BMBbb (HHV) Duct Burner VOC (as CH4), BMBbb (HHV) Duct Burner VOC (as CH4), BMBbb (HHV) Duct Burner HOS, DMBbb (HHV) Duct Burner PHIO, BMBbb (HHV) Duct Burner PHIO, BMBbb (HHV) Duct Burner PHIO, BMBbb (HHV) Total SO2, Bbh from Duct Burner, voffs Total SO2, Bbh from Duct Burner, voffs Total SO3, Bbh from Duct Burner Fuel only (after SO2 addition) Total SO3, Bbh From Duct Burner Fuel only (after SO2 addition) DB NOs, Bsh BB VOC (as CH4), Bsh	499.6 564.2 24,000 20,816 23,091 0,000 73,73,705 24,011 0,6111 1,6111 0,005 0,000 0,	499.6 554.2 24.000 20,816 23,091 0.00% 73,79% 24.01% 0.01% 10.0% 10.0% 0.000 0	471.3 522.8 22.840 20.816 23.091 0.00% 73.78% 24.01% 0.005% 10.00% 0.000	498.3 582.8 23,940 20,916 23,001 0,005 73,785 24,01% 0,016 10,0% 0,000 0	491.7 545.4 23,870 23,870 23,001 0,005, 73,775, 0,015, 0,005, 0,000 0,00	499.5 554.2 24,000 20,815 23,091 0,00% 73,79% 0,01% 0,01% 0,00% 0,000 0,	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0
Duct Burner Flast Input, MSbuft (LHV) Duct Burner Hest Input, MSbuft (LHV) Total Duct Burner Hest Input, MSbuft (LHV) Total Duct Burner Fuel LHV, Bbufb Duct Burner Fuel LHV, Bbufb Duct Burner Fuel LHV, Bbufb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 N7 O2 S Total Feet Suffer Content (grains/100 standard cubic feet) S Duct Burner MO, BMBbb (HHV) Duct Burner LNG (see HH), BMBbb (HHV) Duct Burner MO, BMBbb (HHV) Duct Burner MO, BMBbb (HHV) Duct Burner MO, BMBbb (HHV) Duct Burner MO (see CHH), BMBbb (HHV) Duct Burner MO (see CHH), BMBbb (HHV) Duct Burner MO (see CHH) for fair and seek half catch) Assumed SC2 oddation rate in Duct Burner, woffs Total SO2, Bnh from Duct Burner Fuel only (after SO2 oddation) Total SO3, Bnh from Duct Burner Fuel only (after SO2 oddation) DB NOs, Bnh DB CO, Bnh DB UHC (see CHH), Bnh	499.8 554.2 24,000 20,816 23,091 0,005 73,75% 24,01% 0,15% 0	499.6 554.2 24.000 20,816 23,091 0.00% 73,79% 24.01% 0.01% 10.0% 10.0% 0.000 0	471.3 \$22.8 22.840 2.091 0.0095 73.78% 24.01% 0.00557% 1.01% 0.00057% 1.00% 0.0000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0	496.3 582.8 23.940 20.916 23.001 0.00557 1.015 0.00557 1.00.05 0.006	491.7 545.4 22.650 20.816 23.001 0.00% 73.76% 24.01% 0.0057% 1.01% 0.00607% 0.0000 0.0000 0.0000 0.0000 0.0000 0.0	499.6 554.2 24.000 20.816 23.091 0.00% 73.78% 24.01% 0.01% 0.00% 1.00% 0.000 0	0.0 0.0 0.0 0.0 20,816 23,091 24,015 0.005578 1.015 1.005578

1/14/2006							
FMPA							
Treesure Coast Energy Center Unit 1 Black & Vestch Project 132969.0030							
1x1 Emissions Estimates							
Case Number	1	2	3	4	5	6	7
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type	Natural Ges	Distillate	Natural Gas	Distilitate	Natural Gas	Oistillate	Natural Gas
CTG Load	100%	100%	100%	100%	100%	100%	100%
CTG Inlet Air Cooling	Evap. Cooler	Evap. Cooler	Off	Off	Evap. Cooler	Evap. Cooler	Evap. Cooler
CTG Steam-Water Injection	No	Water 100	No.	Water	No	Water	No
Ambient Temperature, F HRSG Duct Firing	100 Fired	Fired		26 Fired	73 Fired	73 Fired	100 Unfired
Fuel Suffur Content (grains/100 standard cubic feet)	2.00	568.31	2.00	568.31	2.00	566.31	2.00
Stack Errissions							
Stack Exhaust Analysis - Volume Basis - Wet	Law School Physics	0.0000000000000000000000000000000000000	ADBIACO / CONTRACTOR	1000 No. 100 N	394/1542/2/2000/00/55	AT SECTION SECURITY OF	COMPANY TO A CO.
	0.90%	0.86%	0.93%	0.88%	0.91%	0.87%	0.91%
C02	4.86% 12.95%	6 35% 15.83%	4.69% 9.55%	5.21% 13.37%	4.81% 11.59%	6.32%	3.69% 10.71%
N2	12.95%	15.83%	74.10%	70.47%	72.60%	14.93% 69.33%	72.44%
02	9.71%	8.30%	10.73%	9.06%	10.09%	8.55%	12.25%
SO2 (after SO2 oxidation)	0.000120%	0 000060%	0.000120%	0.000050%	0.000120%	0.000060%	0.000090%
SO3 (after SO2 oxidation)	0.000040%	0.000020%	0.000040%	0.000010%	0.000040%	0.000020%	0.000040%
Total	100,0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%
Stack Exit Temperature, F	168	250	157	252	168	251	184
Stack Diameter, ft (estimated)	18	18	18	18	18	18	18
Stack Flow, lb/h	3,380,996	3,506,998	3,856,636	4,027,938	3,529,616	3,674,998	3,356,997
Stack Flow, acfm	783,543	795,505	860,031	904,944	792,988	830,550	754,766
Stack Flow, actm	923,577	1,086,586	1,036,793	1,239,934	958,292	1,135,575	934,925
Stack Exit Velocity, ft/s	60.0	71.0	68.0	B1.0	63.0	74.0	61.0
	\$200 \$ 05 (ACC) (C)	CONTROL OF ACTUAL	200 C	2018/2018/2018/2018/2018/2018/2018/2018/	23 8 9 9 9 9 8 9 2 2	7.84	103000 SA 103
NOx, pprived (dry, 15% O2)	12.3	37.6 69.9	11.9	38.1	12.2	37.8	9.0
NOx, ppmvd (dry) NOx, ppmvv (wet)	20.2 17.6	58.9	18.1 18,4	68.9 58.0	19.5 17.2	69.1 58.8	10.9
NOx, byh as NO2 (includes correction adder)	99.3	344.3	103.8	386.2	100.6	359.3	55.0
NOx, Ib/MBtu (LHV) as NO2 (incl. duct burner fuel)	0.0499	0.1578	0.0480	0.1597	0.0492	0.1586	0.0369
NOx, tb/MBtu (HHV) as NO2 (incl. duct burner fuel)	0.0450	0.1466	0.0433	0.1487	0.0444	0.1475	0.0333
Stack HOx Emissions with the Effects of Selective Catalytic Reduction (SCR)		28.7073.80%X2.204		AND CONTRACTOR	44,000 (27,000)		SPECIAL CONTRACTOR
MOx, pprind (dry, 15% O2)	2.0	8.0	2.0	8.0	2.0	8.0	2.0
NOx, ppmvd (dry)	3.3	14.9	3.0	14.1	3.2 2.8		2.4
NOx, ppmw (wet) NOx, fb/h as NO2 (includes NOx margin applied to CTG)	16.1	73.2	17.5	81.1	16.5		12.2
NOx, fo/MBtu (LHV) as NO2 (incl. duct burner fuel)	0.0081	0.0335	0.0081	0.0336	0.0081	0.0336	0.0082
NOx, tb/MBtu (HHV) as NO2 (Incl. duct burner fuel)	0.0073	0.0312	0.0073	0.0312	0.0073		0.0074
SCR NH3 stip, pprmvd (dry, 15% O2)	10.0	5.0		5.0	10.0		10.0
SCR NH3 stip, to/h	29.4	16.8	31.9	18.6	30.2	17.4	22.0
Stack CD Brisslens	SAME TO ANALYSIS	1000 TO 1000 TO 1000	Karring garden	DOSES SLAVY NAMES	more, comme	MARK 42000 S. C. C.	\$465.0000 PERSON
CO, pprrvd (dry, 15% O2)	10.1	14.9	9.9	15.1	10.1		7.4
CO, pprivid (dry)	16.6	27.7	15.2	26.6	16.1		9.0
CO, ppmww (wet)	14,5	23.4	13.7	23.0			8.0
CO, Ib/h (Includes CO margin applied to CTG)	49.2 0.0247	82.3 0.0377	52.3 0.0242	92.4	50.1		27.0
CO, Ib/MBtu (LHV) (Incl. duct burner fuel) CO, Ib/MBtu (HHV) (Incl. duct burner fuel)	0.0247	0.0350	0.0242	0.0356	0.0245 0.0221		0.01B1 0.0163
	0.0223				3.0221	0.0354	2.0163
Stack 602 Emissions, after 602 Oxidation	40888888888888	is estimated to	を対ける機能は複数	Antalog (State Antalog	1940.07 (1/1960)	ONE SHOW OF COMMA	Marie 1985
Assumed SO2 coddation rate in CO Catalyst, vol's	0.0%			0.0%			0.0%
Assumed SO2 coddstion rate in SCR, vol%	3.0%	3.0%	3.0%	3.0%	3.09	3.0%	3.0%
SO2, ppmvd, (dry, 15% O2)	0.84	0.37	0.84	0.35	0.84	0.36	0.79
SO2, pprind (dry)	1.38						0.96
SO2, ppriver (wet)	1.20	0.58	1.15	0.54			0.86
SO2, Ibrh	9.32	4.68	10.05	4.94	9.55	4.77	6,57
SO2, Ib/MBtu (LHV)_(Incl. duct burner fuel)	0.0047	0 0021		0.0020	0.0047	0.0021	0.0044
SO2, Ib/MBtu (HHV) (incl. duct burner fuel)	0.0042	0.0020	0.0042	0.0019	0.0042	0.0020	0.0040

1/14/2005	

Treasure Coast Energy Center Unit 1
Black & Vestch Project 138889,0030
1x1 Emissions Estimates

Case Number	1	2	3	4	5	6	7
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type	Natural Gas	Distillate	Natural Gas	Distillate	Natural Gas	Distillate	Natural Gas
CTG Load	100%	100%	100%	100%	100%	100%	100%
CTG Intel Air Cooling	Evap. Cooler	Evap. Cooler	Off	Off	Evap. Conter	Evap. Cooler	Evap. Cooler
CTG Steam/Water Injection	No	Water	No	Water	No	Water	No
Ambient Temperature, F	100	100	26	26	73	73	100
HRSG Duct Firing	Fired	Fired	Fired	Fired	Fired	Fired	Unfired
Fuel Sulfur Content (grains/100 standard cubic feel)	2.00	566.31	2.00	566.31	2.00	566.31	2,00

Stack Emissions - command							
Stack UHC Emissions	+256680 TERROR	\$66.000 me (2005)	SARAMA NAKATAN	440000000000000000000000000000000000000	90000000000000000000000000000000000000	VC-27X-576860000000	24.800.000.000
UHC, pprivid (dry, 15% O2)	16.8	15.0	15.4	14.0	16.4	14.6	6.5
UHC, ppmvd	27.7	27.8	23.6	24.7	26.2	26.7	7.8
UHC, ppmww	24.1	23.4	21.3	21.4	23.2	22.7	7.0
UHC, fb/h as CH4 (includes correction adder)	46.7	47.3	48.5	49.2	46.7	48.3	13.4
UHC, Ib/MBtu (LHV) (incl. duct burner fuel)	0.0234	0.0216	0.0215	0.0203	0.0229	0.0213	0.0090
UHC, Ib/MStu (HHV) (Incl. duct burner fuel)	0.0211	0.0201	0.0194	0.0189	0.0206	0.0198	0.0081
Black VOC Britistions	3890 or 41,000 to 5	LANGER CONTRACTOR				Landa Daniel State	3.75
VOC, ppmvd (dry, 15% O2)	1.8	2.9	1.7	2.9	1.7	2.9	1.3
VOC, ppmrd (dry)	2.9	5.4	2.6	5.1	2.8	5.3	1.6
VOC. ppmvw (wet)	2.5	4.6	2.3	4,4	25	4.5	1.4
VOC, Br/n as CH4 (Includes VOC correction as applied to CTG)	4.9	9.2	5.1	10.2	5.0	9.7	2.7
VOC, Ib/MBtu (LHV) (Inct. duct burner fuel)	0.0025	0.0042	0.0024	0.0042	0.0024	0.0043	0.0018
VOC, Ib/MBtu (HHV) (Incl. duct burner fuel)	0.0022	0.0039	0.0021	0.0039	0.0022	0.0040	0.0018
PN10 without the Effects of SO2 criterion	Militarion / March	31000000000000000000000000000000000000	v company	21270xX6V22634E	104400000000000000000000000000000000000		350000000000000000000000000000000000000
PM10 Emissions - Front Half Catch Only							
PM10, byh	14.5	22.5	14.2	22.5	14.5	22.5	9.0
PM10. IbMBtu (LHV) (incl. duct burner fuel)	0.0073	0.0103	0.0066	0.0093	0.0071	0,0099	0.0060
PM10, Ib/MBtu (HHV) (incl. duct burner fuel)	0.0066	0.0098	0.0059	0.0067	0,0064	0.0093	0.0054
PM10 Emissions - Front and Back Half Catch							
PM10, but	31.3	47.3	30.5	47.3	31.1	47.3	18.0
PM10, IbMBtu (LHV) (incl. duct burner fuet)	0.0157	0.0217	0.0141	0.0195	0.0152	0.0209	0.0121
PM10, lb/MBtu (HHV) (incl. duct burner fuel)	0.0142	0.0201	0.0127	0.0182	0.0137	0.0194	0.0109
PM10 with the Effects of SC2 Oxidation [includes (HH4)2-(SO4)]	96: 40:3388888	Q160-05-0-199-05-028	254,000000000000000000000000000000000000	SECRETARY OF SEC	22.00	4520 00000000000000000000000000000000000	A CONTRACTOR
PM10 Emissions - Front Half Catch Only							
PM10, Ibih	14.5	22.5			14.5	22.5	9.0
PM10, Ib/MBtu (LHV) (Inci. duct burner fuel)	0.0073	0.0103	0.0068	0.0093	0.0071	0.0099	0.0060
PM10, Ib/MBtu (HHV) (incl. duct burner fuel)	0.0086	0.0096	0.0059	0.0087	0.0084	0.0093	0.005
PM10 Emissions - Front and Back Half Catch							
PM10, Ib/h	38.0	49.8	38.0	50.0	38 0	49.9	23.8
PM10, Ib/MBtu (LHV) (Incl. duct burner fuel)	0.0191	0.0228	0.0176	0.0207	0.0186	0.0220	0.016
PM10, tb/M8tu (HHV) (Incl. duct burner fuel)	0.0172	0.0212	0.0158	0.0193		0.0205	0.014
Trital Effects of SO2 Oxidation	400 F 100 K		8.0000000000000000000000000000000000000	\$55.00 pt 25.00 pt 26.00 pt 2	401470000000000000000000000000000000000	CKAN CAMMIN	AMERICAN STREET
Total SO2 to SO3 conversion rate, %vol	25.6%		26.4%				30.2
Total Amount of SO2 converted to SO3, b/h	3.24						2.8
Maximum Stack Ammonium Sulfate [(NH4)2-(SO4)] (assuming 100% conversion from SO3), fb/h	5.67	2.54	7.42	2.78	6.90	2.63	5.8
Maximum Stack H2SO4 (assuming 100% conversion from SO3 to H2SO4), tb/h	4.95	1.89	5.50	2.06	5.12	1.95	4.3
		<u> </u>	ı			ı	0

nbustion Emissions Control Equipment

Selective Catalytic Reduction (SCR)	REST CONSISTS AND AND ASSESSMENT	80.00 PEG 1. (CASSES	AUSTRONOMIC	485000000000000000000000000000000000000	STATE OF THE STATE	De Marie Control	80,880 S S S S S S S S S S S S S S S S S S
NOx Removed in SCR, %wt	63.8%	78.8%	83.2%	79.0%	63.6%	78.8%	77.8%
NOx removed in SCR, florin	B3.2	271.2	86.4	305.1	84.1	283.3	42.8
Arrenonia Stip, #brh	29.4	16.8	31.9	18.6	30.2	17.4	22.0
				1			

- The emissions estimates shown in the table above are per stack.
 The dry air composition used is 0.99% Ar, 78.00% N2 and 20.99% O2
 Standard conditions are defined as 60 F, 14,696 paia, Norm conditions are defined as 0 C, 1,103 bar.

- 3. Standard conditions are defined as 00 F. 14 (600 pass, Norm conditions are defined as 0 C. 1.103 bat
 4. All print values are based on CH catibration pass.
 5. The CTG aperformance is from GTP, a General Electric estimation program.
 6. The HZO increase in the SCR catalyst is negligible and not included in the analysis.
 7. The VCC/LHC ratio is assumed to be 20% for NG and 50% for distillate.
 8. Ammonium suffates created downstream of the SCR are included in the back half particulates. The essumption that 100%
 SO3 is converted to ammonium suffates results in "worst cases" particulate emissions.
- 9. Where manufacturer data of bih of poliutari emissions were evaluable, the greater of the manufacturer's estimate and 84Vs estimate was used in the summary table, i.e. the 88V estimates were addusted, where applicable,

 10. Duct burner emissions are included. The duct burner poliutard emissions are Black & Vestich estimates based on low NOx duct burner emissions data (provided by Former).
- The front half catch of CT perticulate emissions is assumed to be half the amount of the front and back half catch.
 As requested the SCR was designed to reduce the NOx stack emissions to 2 and 8 permitight 15%O2 when firing NG and Destitate, respectively.
 The emissions estimate is based on FGT gas with a maximum subtur content of 2.0 prainar100scr,

1/14/2006						<u> </u>	
FMPA Treasure Coast Energy Center Unit 1							
Black & Vestch Project 138859.0030					l		
121 Emissions Estimates Case Number	8 }	9	10	11	12	13	14
			.,		"	" _	
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type CTG Load	Oistillate 100%	Natural Gas 100%	Distitate 100%	Matural Gas 100%	Distillate 100%	Natural Gas 75%	Oistillate 75%
CTG Intel Air Cooling	Evap. Cooler	Off	Off	Evap. Cooler	Evap. Cooler	Off	ON
CTG SteamWater Injection Ambient Temperature, F	Water 100	No 26	Water 26	No. 73	Water 73	No. 100	Weter 100
HRSG Duct Firing	Unfired	Unfired	Unfired	Unfired	Unfired	Unfired	Unfired
Fuel Sulfur Content (grains/100 standard cubic feet)	568.31	2.00	566.31	2.00	566,31	2.00	566 31
Ambient Conditions					1		
	·-··-						
Ambient Temperature, F	100.0	26.0	26.0	73.0	73.0	100.0	100.0
Ambient Relative Humidity, % Almospheric Pressure, psia	48.4 14.690	100.0	100.0	81.5 14.690	81.5	48.4 14.690	48.4 14.690
Combustion Turbine Performance							
CTG Performance Reference	GTP	GTP	GTP	GTP	GTP	GTP	GTP
CTG Inlet Air Conditioning Effectiveness, % CTG Compressor Inlet Dry Burb Temperature, F	85.2 85.2	0 26.0	0 26.0		8S 69,5	100.0	100.0
CTG Compr. Inlet Relative Humidity, %	89.7	100.0	100.0	97.0	97.0	48.5	48.5
	- 40		40			40	
Intel Loss, in. H2O Exhaust Loss, in. H2O	4.0	4.0 16.7	4.0	14.3	4.0 15.4	4.0 8.6	9.3
CTG Load Level (percent of Base Load) Gross CTG Output, MV	100%	100% 183,500	191,000	100%	100% 173,200	75% 108,400	75%
Gross CTG Heat Rate, SturkWh (LHV)	10,310	9,220	10,050	9,480	10,200	10,900	11,540
Gross CTG Heat Rate, BtufkWh (HHV)	10,980	10,228	10,704	10,516	10,863	12,091	12,290
CTG Hest Input, MBtufh (LHV)	1,684.7	1,591.9	1,919.6	1,552.8	1,786.6	1,181.6	1,339.8
CTG Heet Imput, MBturh (HHV)	1,794.2	1,876.8	2,044.4	1,722.5	1,881.5	1,310.7	1,426.9
CTG Water/Steam Injection Flow, Joh	109,030		143,570	0	122,910	0	80,680
Injection Fluid/Fuel Ratio	1.2	0.0		0.0	1.3	0.0	1.1
CTG Exhaust Flow, Ib/h	3,483,000	3,834,000	4,004,000	3,506,000	3,651,000	2,688,000	2,785,000
CTG Exhaust Temperature, F	1,135	1,082	1,080	1,129	1,113	1,198	1,195
Companion Turbine Firet	TOWN A PARESTON	National Services	255000000000000000000000000000000000000	NAMES OF STREET			ereged to accept the
Total CTG Fuel Flow, b/h	92,080	81,260	104,890	74,600	96,540	56,760	73,210
CTG Fuel Temperature, F	60	365	60	365		365	60
CTG Fuel LHV, Btu/lb	18,300	20,816	18,300	20,816	18,300	20,816	18,300
CTG Fuel HHV, Bhufb	19,490	23,091	19,490	23,091	19,490	23,091	19,490
HHV/LHV Ratio	1.0650	1.1093	1,0650	1.1093	1.0850	1,1093	1,0650
CTG Fuel Composition (Ultimate Analysis by Weight)							
<u> </u>	0.00%	0.00%	0.00%	0.00%	0.00%	0.00%	0.00%
С	85.00% 14.80%	73.76%	85.00% 14.80%	73.76% 24.01%	85.00% 14.80%	73.76% 24.01%	85.00% 14.80%
N2	0.20%	0.61%	0.20%	0.61%	0.20%	0.61%	0.20%
9	0.00% 0.00150%	1.61% 0.00657%	0.00%	1.61% 0.00657%	0.00%	1.61% 0.00657%	0.009
Total	100.00%	100.00%	100.00%	100.00%	100.00%	100.00%	100.00%
Fuel Suffur Content (grains/100 standard cubic feet)	566.31	2.00	566.31	2.00	566.31	2.00	566,31
Combustion Turbine Exhaust							
			~~~				
CTG Exhaust Analysis (Votame Bests - Wel)	0.87%	0.94%	0.89%	0.92%	0.88%	0.91%	0.889
C02	5.24%	3.71%	5.24%	3.69%	5.26%	3.56%	5,239
H20	13.72%	7.65%	11.49%	9.46%	12.90%		
N2 02	69.45% 10.72%					10.14%	12.889
SO2, (after SO2 cookston)	0.00003%		71.18% 11.19%	73.42%	70.10%	10.14% 72.86%	70,101
SO3, (after SO2 coddation) Total			11.19% 0.00003%	12.50% 0.00010%	70.10% 10.67% 0.00003%	10.14% 72.86% 12.43% 0.00010%	70.104 10.911 0.000031
	0 00001%	0.00010%	11.19% 0.00003% 0.00001%	12.50% 0.00010% 0.00002%	70.10% 10.67% 0.00003% 0.00001%	10.14% 72.86% 12.43% 0.00010% 0.00002%	70.10* 10.91* 0.000031 0.00001*
	0.00001%	0.00010% 0.00002% 100.0%	11.19% 0.00003% 0.00001% 100.0%	12.50% 0.00010% 0.00002% 100.0%	70.10% 10.67% 0.00003%	10.14% 72.86% 12.43% 0.00010%	70,104 10,911 0,000031 0,000011
Molecular W1, Birmol	0 00001% 100.0% 28.01	0.00010% 0.00002% 100.0%	11.19% 0.0003% 0.00001% 100.0%	12.50% 0.00010% 0.00002% 100.0%	70.10% 10.57% 2.00003% 0.00001% 100.0%	10.14% 72.85% 12.43% 0.00010% 0.00002% 100.0%	70.104 10.911 2.000001 0.000011 100.04
Molecular W1, Bitnol Specific Volume, P1976	0.00001%	0.00010% 0.00002% 100.0%	11.19% 0.00003% 0.00001% 100.0%	12.50% 0.00010% 0.00002% 100.0% 28.27 39.85	70.10% 10.67% 2.00023% 0.00001% 100.0%	10.14% 72.85% 12.45% 0.00010% 0.00002% 100.0% 28.19 42.06	70.10/ 10.91* 0.000001 0.00001 100.0* 28.11 42.0
Melecular WI, Ehmol Specific Volume, PL'97b Specific Volume, act/fb Ehaust Gas Flow, act/m	0 00001% 100.0% 28.01 40.18 13.54 2,332,449	0,00010% 0,00002% 100,0% 28,47 37,99 13,33 2,427,561	11.19% 0.00003% 0.00001% 100.0% 28.26 37.61 13.43 2,509.841	12.50% 0.00010% 0.00002% 100.0% 28.27 39.65 13.42 2,316,882	70.10% 10.97% 2,00003% 0,00001% 100.0% 28.11 39.38 11.50 2,396.273	10.14% 72.86% 12.43% 0.00010% 0.00002% 100.0% 28.19 42.06 13.46 1,884,288	70.10* 10.91* 0.00003* 0.00001* 100.0* 28.10 42.0 13.50 1.951,355
Molecular Wt, Britrol Specific Volume, M'S/Ib Specific Volume, actib	0 00001% 100.0% 28.01 40.18 13.54	0.00010% 0.00002% 100.0% 28.47 37.99	11.19% 0.00003% 0.00001% 100.0% 28.26 37.61 13.43	12.50% 0.00010% 0.00025% 100.0% 28.27 39.65	70.10% 10.87% 0.00003% 0.0001% 100.0% 28.11 39.38	10.14% 72.85% 12.45% 0.00010% 0.00002% 100.0% 28.19 42.06	70,104 10,915 0,000001 0,00001 100,04 28,10 42,04 13,55 1,951,357
Melecular WI, Ehmol Specific Volume, PL'97b Specific Volume, act/fb Ehaust Gas Flow, act/m	0 00001% 100.0% 25.01 40.15 13.54 2,332,449 765,997	0.00010% 0.00002% 100.0% 28.47 37.99 13.33 2,427,551 851,787	11.19% 0.00003% 0.00001% 100.0% 28.26 37.61 13.43 2,509.841	12.50% 0.00010% 0.00002% 100.0% 28.27 39.65 13.42 2,316,882	70.10% 10.97% 2,00003% 0,00001% 100.0% 28.11 39.38 11.50 2,396.273	10.145 72.85% 12.45% 0.00010% 100.00% 100.00% 100.00% 11.460 11.664.280 603,008	70,109
Molecular W4, Brind Specific Volume, in 1976 Specific Volume, actflb Echaust Gas Flow, actm Echaust Gas Flow, actm	0 00001% 100.0% 25.01 40.15 13.54 2,332,449 765,997	0.00010% 0.00002% 100.0% 28.47 37.99 13.33 2.427,561 851,787	11.19% 0.00003% 0.00001% 100.0% 28.26 37.61 13.43 2,509,841 896,229	12.50% 0.00012% 0.0002% 100.0% 28.27 39.65 13.42 2.316,862 784,175	70.10% 10.57% 2.000031% 0.00001% 100.0% 28.11 30.36 13.50 2.386.273 821.475	10.14% 72.65% 12.45% 0.00010% 100.00% 100.00% 100.00% 128.19 42.06 13.46 1,884,288 603,008	70,104 10,941 0,000007 0,000011 100,07 28,15 42,0 13,56 1,951,355 628,62
Melecular WI, Ehmol Specific Volume, PL*VIb Specific Volume, PL*VIb Specific Volume, act/fib E-thaust Gas Flow, act/m E-thaust Gas Flow, act/m E-thaust Gas Flow, act/m E-thaust Gas Flow, act/m Additional Percent Margin Included in mass based NOx Emissions below	0 00001% 100 0% 28.01 40.15 1354 2.332,449 785,997	0,00010% 0,00021% 100,0% 28,47 37,99 13,33 2,427,561 851,797	11,19% 0,0000% 0,00001% 100,0% 28,25 37,91 13,43 2,509,841 896,229	12 50% 0 00010% 0 00002% 100.0% 28.27 39.65 13.42 2.316,882 784,175	70 10% 10.87% 0.00003% 0.00001% 100.0% 100.0% 133.86 135.0 2.386.273 821.475	10.14% 72.85% 12.45% 0.00007% 0.00002% 100.07% 12.13.45% 13.84.258 603.006	70 100 10 10 10 10 10 10 10 10 10 10 10 1
Molecular W1, Ehmol Specific Volume, h*3/b Specific Volume, sc/fib Specific Volume, sc/fib Eshaust Gas Flow, sc/m Eshaust Gas Flow, sc/m Eshaust Gas Flow, sc/m CTO NOx Emissions (Without Post Combustion Emissions Control)	0,00001% 100,0% 28,011 40,18 1354 2,232,440 785,997 0% 42,000 66,000	0,00010% 0,00021% 100.0% 28,47 37,99 13,33 2,427,561 651,787 0% 9,00	11.19% 0.00009% 0.00001% 100.0% 28.25 37.61 13.43 2.509,841 898,229 0% 42.00	12 5050% 0 000012% 0 00002% 100.0% 28.27 39.65 13.42 2.316,862 784,175	70.10% 10.87% 0.00007% 0.00007% 10.00% 100.0% 28.11 39.36 13.50 2.386.273 821.475 0% 42.00 59.70	10.14% 72.85% 12.45% 0.00010% 0.00025% 100.0% 28.19 42.06 13.46 603,000 0%	70.10* 10.00* 10.00001* 100001* 10000* 100001* 10000* 28.16* 42.0* 13.5* 1,891.36* 628.62*
Melecular WI, Ehmol Specific Volume, A**2/b Specific Volume, act/fb Especific Volume, act/fb Especific Specific	0 00001% 100.0% 28.01 40.18 1354 2,332,440 785,997 0%	0,00010% 0,00007% 100.0% 28.47 37.99 13.33 2,477,561 651,761 0% 9.00 10.600	11.19% 0.00001% 0.0001% 100.0% 28.25 37.91 13.43 2.559,841 985,229 6% 42.00 58.50 51.80	12 50% 0 00010% 0 00002% 100.0% 28 27 39.65 13-42 2.316.862 784.175 0% 8.00 10.80	70 10% 10.87% 0.00001% 0.00001% 100.0% 100.0% 13.38 13.50 2.388.273 821,475 0% 42.00 99.70 55.20	10.11% 72.85% 12.45% 0.00017% 0.000027% 100.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07% 120.07	70 199 10 2000 10 2000 11 10 20 20 20 20 20 20 20 20 20 20 20 20 20
Molecular WI, Brind Specific Volume, In*1/16 Specific Volume, In*1/16 Specific Volume, act/16 Enhant Gas Flow, act/m Enhant Gas Flow, act/m Enhant Gas Flow, act/m Additional Percent Margin included in mass based NOx Emissions below  NOx, germed (dn), 15% CO; NOx, pormed (dn)	0,00001% 100,0% 28,011 40,18 1354 2,232,440 785,997 0% 42,000 66,000	0,00010% 0,00007% 100.0% 28.47 37.99 13.33 2,477,561 651,761 0% 9.00 10.600	11.19% 0.00009% 0.00001% 100.0% 28.25 37.61 13.43 2.509,841 898,229 0% 42.00	12 50% 0 00010% 0 00002% 100.0% 28 27 39,65 13-4 2,318,862 784,175 0%	70.10% 10.87% 0.00007% 0.00007% 10.00% 100.0% 28.11 39.36 13.50 2.386.273 821.475 0% 42.00 59.70	10.11% 72.85% 12.45% 0.00017% 0.000027% 100.07% 120.15% 1,584.280 603,000 605,000 9.00 10.800 9.00	70.10** 10.93** 0.00000** 0.00000** 1000** 1000** 28.11 20.1 3.55 1.951.35 0.8.62** 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0
Melecular WI, Brind Specific Volume, It'3/D Specific Volume, It'3/D Specific Volume, It'3/D Specific Volume, settle Echanat Gas Flow, settle Echan	0,00001% 100,0% 28,01 40,16 1354 2,232,449 785,897 00% 42,00 60,00 51,00 300,0	0,00010% 0,00021% 100,0% 28,47 37,99 13,33 2,427,561 651,767 7% 9,00 9,00 9,00 9,00 9,00 9,00	11.19% 0.00003% 0.00001% 100.0% 28.26 37.61 13.43 2.509,841 696,229 0% 42.00 59.50 51.80	12 50% 0 00010% 0 00002% 100 0% 120 27 39 85 13 42 2,316,882 784,175 0% 9 9 00 10 80 9 78	70.10% 10.57% 0.00007% 0.00007% 100.0% 100.0% 128.11 30.38 1.350 2.398.273 821.475 0% 42.00 99.70 52.00 335.0	10.14% 72.85% 12.45% 0.00010% 0.000027% 100.0% 28.19 42.06 13.46 1.884,288 603,008	70.10** 10.000000 0.000001 10000 100001 10000 28.1.1 42.0 13.3.5 628.62 0 42.0 53.3 51.7 52.6 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63.62 63
Melecular WI, Ehmol Specific Volume, PL*Vib Specific Volume, PL*Vib Specific Volume, pt*Vib Specific Volume, pt*Vib Specific Volume, pt*Vib Specific Volume, pt*Vib Enhant Gas Flow, actin Enhant Gas Flow, actin  CTO NOX Emissions (Mithout Post Combustion Emissions Control) Additional Percent Margin Included in mass based NOX Emissions below  NOX, pprovid (dry, 15% OZ) NOX, pprove (vert) NOX, pprove (vert) NOX, pprove (vert) NOX, ph/Rsu (LHV) NOX, bh/Rsu (LHV) NOX, bh/Rsu (LHV)	0,0001% 100.0% 100.0% 40.18 1354 2,332,440 785,987 0% 42,00 60,00 51,80 300,0 0,1781	0.00010% 0.00002% 100.0% 100.0% 28.47 37.99 13.33 2.427.561 651,767 0% 9.00 10.50 9.00 0.0066 0.00300	11.19% 0.00001% 0.0001% 100.0% 28.26 37.61 13.43 2.509.841 696.29 695.29 695.39 42.00 595.50 51.80 342.0 0.1782	12 50% 0 00010% 0 00002% 100.0% 28 27 7 39 65 13-4 2 316.882 784.175 0% 9.00 10.90 9.50 9.57 0.0331	70.10% 10.87% 0.00007% 0.00007% 10.00% 100.0% 100.0% 135.0 2.386,273 821,475 0% 42,00 59,70 \$2,00 315.0 0.1783 0.1674	10.14% 72.85% 12.45% 0.00017% 10.00027% 100.07% 28.19 42.06 1.13-68 603.000 0% 9.00 10.80 9.70 430 0.00046	70.10** 10.00** 10.00001** 10.00001** 10.0001** 10.0001** 28.16** 42.0** 1.551.35** 628.62** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0** 42.0**
Melecular W1, Ehmol Specific Volume, Pt*Vib Enhant Gas Flow, actin Enhant Gas Flow, actin Enhant Gas Flow, actin CTO NOX Emissions (Mithout Post Combustion Emissions Control) (251, 1987) (4859-4879) (2707) Additional Percent Margin Included in mass based NOX Emissions below NOX, ppmof (dry, 15% OZ) NOX, ppmof (dry) NOX, ppmer (vert) NOX, pbm as NOZ NOX, pbMss (NOZ) NOX, pbMss (NOZ) NOX, pbMss (NOZ)	0,0001% 100.0% 100.0% 40.18 1354 2,332,440 785,987 0% 42,00 60,00 51,80 300,0 0,1781	0,00010% 0,00007% 100,0% 28,47 37,99 13,33 2,427,561 651,787 CHARMER SENT,787 CHARMER SENT,	11.19% 0.00001% 0.0001% 100.0% 28.25 37.91 13.43 2.559,841 985,229 9% 42.00 55.50 51.80 342.0 0.1782 0.1673	12 50% 0 00010% 0 00002% 100.0% 120.77 39.65 13-42 2.316.862 784.175 0% 8.00 10.80 9.90 9.90 0.0331	70.10% 10.57% 0.00007% 0.00007% 10.00% 10.00% 28.11 39.38 13.50 2.386.273 821.475 0% 42.00 59.70 52.00 1.1763 0.1674	19.14% 72.85% 12.45% 0.00010% 100.00% 100.00% 100.00% 128.19 42.05 13.46 1,894.288 603,008 9.00 10.80 9.00 10.80 9.00 0.0384	70.190 10.091 10.00001 10.00001 10.00001 10.000 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50 13.50
Melecular WI, Ehmol Specific Volume, PLYIB Echaust Gas Flow, actim Echaust Gas Flow, actim Echaust Gas Flow, actim CTO NOX Emissions (Without Post Combustion Emissions Control) Additional Percent Margin Included in mass based NOX Emissions below  NOX, pprint (ptr) NOX, ppmid (ptr) NOX, ppmid (ptr) NOX, ppmid (ptr) NOX, pbm is NO2 NOX, pht/Bib (URV) NOX bh/Bib (URV)	0 00001% 100.0% 28.01 40.18 1354 2.332,440 765,997 0% 4.200 650.00 51.80 300.0 0.1781 0.1672	0,00010% 0,00007% 100.0% 28.47 37.99 13.33 2,427,561 651,797 076,00007% 9,00 10,000 9,00 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006	11.19% 0.00001% 0.0001% 100.0% 28.26 37.61 13.43 2.509.841 696.229 6% 42.00 58.50 51.80 342.0 0.1762 0.17673	12 50% 0 000010% 0 00002% 100.0% 23 27 39.65 13-4 2,316,882 784,175 0% 9.00 10.80 9.00 9.00 0,0367 0,0331	70.10% 10.57% 10.57% 0.00007% 10.00% 10.00% 10.00% 10.00% 10.00% 10.00% 10.00% 10.00% 10.00% 10.00% 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43.00 0.00544 0.00525	70.10** 10.93** 10.00001** 10.00001** 100.00** 28.11** 29.10** 13.55** 13.55** 50.82** 42.0  0.00** 42.0  13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 13.50** 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Molecular WI, Ehmol Specific Volume, N°-Wb Specific Volume, n°-Wb Specific Volume, n°-Wb Specific Volume, nc/IIb Exhaust Gas Flow, actim Exhaust Gas Flow, actim Exhaust Gas Flow, actim Additional Percent Margin included in mass based NOx Emissions below  NOx, permed (dry, 15% OZ) NOx, permed (dry, 15% OZ) NOx, permed (dry, 15% OZ) NOx, but Shou (LHV) NOx, but Shou (LHV) NOx, but Shou (LHV) NOx, but Shou (LHV) CTQ CO Emissions (Withhout Post Combustion Emissions Control)  Additional Percent Margin included in mass based CO Emissions below  CO, permed (dry, 15% OZ) CO, permed (dry, 15% OZ) CO, permed (dry)	0,00001% 28,01 40,18 13,54 2,332,440 785,867  42,00 60,00 51,80 300,0 1,781 0,1672  114,00 20,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 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173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173,00 173	0,00010% 0,00002% 100.0% 28,47 37,99 13.33 2,427,561 651,787 0% 9,00 10,60 9,00 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 0,0006 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821,475 0% 42.00 59.70 52.00 315.0 0.1783 0.1783 0.1783	10.11% 72.85% 12.45% 0.00017% 10.00% 10.00% 28.19 42.06 1.1.46 1.894.288 603.008 0% 9.00 10.80 9.70 4.30 0.00544 0.00328	70.10** 70.10** 10.00007* 0.000007* 10000* 10000* 28.16** 29.11** 1,981.35** 628.62** 20. 42.0** 53.3** 51.7** 23.68** 0.176** 0.165** 0.174** 0.165** 20.0 11.4.2 20.0 11.4.4
Melecular WI, Ehmol Specific Volume, PLYR Specific Volume, settle Exhaust Cas Flow, settle Additional Percent Margin included in mass based NOx Emissions Control NOx, pormed (dry, 15% OZ) CO, pormed (dry, 15% OZ) CO, pormed (dry)	0 00001% 100.0% 100.0% 28.01 40.18 1354 2.323,449 785,897 0% 42.00 60.00 51.00 0.1781 0.1672	0,00010% 0,00007% 100,0% 28,47 37,99 13,33 2,427,561 0% 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 10,500 9,00 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Melecular WI, Birnol Specific Volume, e1795 Specific Volume, e1795 Specific Volume, e1795 Specific Volume, exitib Exhaust Cas Flow, actin  Additional Percent Margin included in mass based NOx Emissions below  NOx, pormet (dry, 15% OZ) NOx, pormet (dry) NOx, pormet (dry) NOx, pormet (dry) NOx, but is NOZ NOx, but is NOZ NOx, but is NOZ NOx, but is NOZ CTQ CO Emissions (Without Post Combustion Emissions Control) Additional Percent Margin included in mass based CO Emissions below  CO, pormet (dry), 15% OZ) CO, pormet (dry), CO, pormet (dry) CO, but is NOZ CO, but	0 00001% 100.0% 28.01 40.18 1354 755,997 785,997 0% 42.00 650.00 511.00 300.0 0.1781 0.1672 0% 14.00 20.00 17.00 10.00357	0,00010% 0,00007% 100,0% 28,47 37,99 13,33 2,427,561 651,787 (**Characteristics** 0,0% 9,00 10,90 9,00 0,000 9,00 0,000 9,00 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 0,000 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Molecular VM, Birnol Specific Volume, M*Mb Specific Volume, M*Mb Specific Volume, editib Exhaust Case Flow, actim Exhaust Case Flow, actim Exhaust Case Flow, actim Additional Percent Margin included in mass based NOx Emissions below  NOx, garmed (dhy, 15% OZ) NOx, pormed (dhy, 15% OZ) NOx, pormed (dhy) NOx, pormed (dhy) NOx, pormed (dhy) NOx, bh/Mbb (HHV)  CTQ CO Emissions (Without Post Combustion Emissions Control) Additional Percent Margin included in mass based CO Emissions below  CO, ppmed (dhy, 15% OZ) CO, ppmed (dhy) CO, ppmed (dhy) CO, ppmed (dhy) CO, ph/Mbb (HHV)  CTQ SO Emissions (After SOZ Oxydetton, Without Post Combustion Emissions Control)  CTQ SOZ Emissions (After SOZ Oxydetton, Without Post Combustion Emissions Control)	0 00001% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 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Molecular VM, Birnol Specific Valuame, PCVB Additional Percent Margin included in mass based NOx Emissions below NOx, pprints (dry, 15% OZ) NOx, pprints (dry) CO, pprint (dry), 15% OZ) CO, pprint (dry), 15% OZ) CO, pprints (dry) SCTQ SCD Emissions (ARtir SOZ Carydistion, Without Post Combisistion Emissions Control) Additional Percent Margin included in this DoS Emissions below Assumed SOZ evidation raths in CTG, vdfs SOZ, pprints (dry, 15% OZ)	0,000014 28,01 40,18 13,54 2,332,440 785,967 0% 42,00 60,00 51,80 3000 0,1781 0,1672 0% 14,00 20,00 17,00 10,0035 0,0035	0,00010% 0,00007% 100,0% 28,47 37,99 13,33 2,427,561 0,0% 9,00 10,50 9,00 10,50 9,50 10,50 9,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 10,50 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Molecular VM, Birnol Specific Valume, PT/NB Exhaust Case Flow, actim Exhaust Case Flow, actim Exhaust Case Flow, actim Exhaust Case Flow, actim Additional Percent Margin included in mass based NOx Emissions below  NOx, pormed (dry), NOx, ppmed (dry) COx, ppmed (dry), LS% OZ) COx, ppmed (dry), LS% OZ) COx, ppmed (dry), LS% OZ) COx, ppmed (dry) COx, ppmed (dry) COx, ppmed (dry) COx, ppmed (dry) Specific Emissions (ARter SOZ Oxydiation, Without Post Combination Emissions Control) Additional Percent Margin included in bih SOZ Emissions below Assumed SOZ coldston rate in CTG, vol% SOZ, ppmed (dry), 15% OZ) SOZ, ppmed (dry)	0,000014 28,01 40,18 1354 2,332,440 7755,967 42,00 60,00 51,80 300,0 0,1781 0,1672 0% 14,00 20,00 17,30 10,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 0,0057 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Molecular WI, Ehmol Specific Volume, N°4/No Specific Volume, ec/th Specific Volume, ec/th Specific Volume, ec/th Exhaust Clas Flow, actim Exhaust Clas Flow, actim Exhaust Clas Flow, actim Additional Percent Margin included in mass based NOx Emissions below  NOx, pormed (dhy, 15% OZ) NOx, pormed (dhy, 15% OZ) NOx, pormed (dhy) NOx, pormed (dhy) NOx, pormed (dhy) NOx, but as NOZ NOx, but as NOZ NOx, but as NOZ NOx, but as NOZ CTQ CD Emissions (Without Post Combustion Emissions Control) Additional Percent Margin included in mass based CO Emissions below  CO, pormed (dhy), 15% OZ) CO, pormed (dhy) SOZ, pormed	0,000019 28.01 40.18 1354 2,232,440 785,897  0% 42.00 63.00 63.00 0,1781 0,1672  0% 00% 14.00 20.00 17.30 60.11 0,0357 0,0355 0,0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 20.0% 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Treesure Coast Energy Center Unit 1 Black & Vestch Project 13888.0030					1		
1x1 Emissions Estimates							
Case Number	8	9	10	11	12	13	14
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type	Distillate 100%	Natural Gas	Distillate	Natural Gas	Distillate	Natural Gas	Distillate
CTG Land CTG triet Air Cooling	Fven Cooler	100%	100%	100% Evap. Cooler	100% Evap, Cooler	75% Off	75% Off
CTG Steam/Water Injection	Water	No.	Water	Evap. Couler	Water	No	Water
Ambient Temperature, F	100	26	26	73	73	100	100
HRSG Duct Firing	Unfired	Unfired	Unfired	Unfired	Unfired	Unfired	Unfired
Fuel Suttur Content (grains/100 standard cubic feet)	566.31	2.00	568.31	2.00	568.31	2.00	566,31
Combustion Turbine Exhaust - continued							
CTG LHC Emissions (Without Post Combustion Emissions Control)	8188838351070 Carl 1988	35.11 (85.7 Ke/0)8	W. C.	275 ( <del>1886</del> / S. 1740 <b>/</b> 188	V 2000 - 2000 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 2000 - 20	1249	375 200 300 300
Additional Percent Margin included in Ib/h UHC Emissions Below	0.0%	0.0%	0.0%	0.0%	0.0%	0.0%	0.0%
UHC, ppmvd (dry, 15% O2)	5.7	6.4	5.7	6.4	5.7	65	5.7
UHC, ppmvd (dry)	8.1 7.0	7.6 7.0	7.9 7.0	7.7	8.0 7.0	7.8 7.0	8.0 7.0
UHC, ppmww (wet) UHC, tb/h as CH4	14.0	15,1	16.0	14.0	15.0	11.0	11.1
UHC, Ib/MBtu as CH4 (LHV)	0.0083	0.0089	0.0083	0.0090	0.0085	0.0093	0.0083
UHC, Ib/MBtu == CH4 (HHV)	0.0078	0.0081	0.0078	0.0081	0.0080	0.0084	0.0078
9-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1	N. S. Saponias		and a second Alberta		VIII. W. X. X. X. V.		
CTG VCC Entestions (Without Post Combustion Emissions Control	WAR CARRES	200		00		SPC/RESE CONTRACTOR	
Additional percent margin included in lb/h VOC emissions below	0%	0%	0%			0%	0%
VOC percentage of UHC	50%	20%	50%	20%	50%	20%	50%
VOC, ppmvd (dry, 15% O2)	2.8	1.3	28	1.3	2.8	1.3	2.8
VOC, ppmvd (dry)	4.1	1.5	4.0	1.5	4.0	1.6	4.0
VOC, pprove (wet)	3.5	1.4	3.5	1.4	3.5	1.4	3.5
VOC, Byth as CH4	7.0 0.0042	3.0 0.0018	8.0 0.0042	2.8 0.0018	7.5 0.0042	0.0019	5.6 0.0042
VOC, Ib/MBtu as CH4 (LHV)  VOC, Ib/MBtu as CH4 (HHV)	0.0039	0.0016	0.0039	0.0016	0.0040	0.0017	0.0042
		0.0010	0.00.0	0.0010	0.000	0.00	Vidual
CTO PM 19 Emissions (without the Effects of SO2 Oxidation)	\$2000 S.M. 1284 1.548	NAMES OF STREET		SELECTION OF THE	18 Sept. 10 Sept. 10	2839 W.	\$1.00 SHEETS
Percent margin included in PM10 emissions below	0%	0%	0%	0%	0%		0%
PM10 Emissions - Front Half Catch Only PM10, Brit	17.0	9.0	17.0	9.0	17.0	9.0	17.0
PM10, IbMBtu (LHV)	0.0101	0.0063	0.0089	0.0058	0.0098	0.0076	0.0127
PM10, Ib/MBtu (HHV)	0,0095	0.0048	0.0063	0.0052	0.0090	0.0069	0.0119
PM 10 Emissions - Front and Back Half Catch							
PM10, lb/h PM10, lb/M8b; (LHV)	34.0 0.0202	18.0 0.0108	34.0 0.0177	18.0 0.0116	34.0 0.0192	18.0	34.0 0.0254
PM10, IDMBtu (HMV)	0.0189	0.0096	0.0166	0.0104	0.0181	0.0137	0.0238
					•		
MRSG Duct Burners							
Quot Burner Fixel	15 TO 10	C1000000000000000000000000000000000000	100000 1000 1000 1000 1000 1000 1000 1	Proteint Proteins	2022 X A S ( S )	THE TO SELECT CHARGE	098405000000000000
Duct Burner Heat Input, MBtu/h (LHV)	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Duct Burner Heat Input, M8tu/h (HHV)	0.0			0.0	0.0		
Total Duct Burner Fuel Flow, to/h	0		0		•	<u> </u>	
	<b>(</b>						
Duct Burner Fuel LHV, Btu/lb	20,816	20,816	20,816	20,816	20,816	20,816	20,816
Duct Burner Fuel HHV, Btu/to	23,091	23,091	23,091	23,091	23,091	23,091	23,091
			ļ				
Duct Burner Fuel Composition (Uttimate Analysis by Weight)  Ar	0.00%	0.00%	0.00%	0.00%	0.00%	0.00%	0,00%
c c	73.76%	73.76%		73.76%	73.76%	73.76%	73.76%
н2	24.01%	24.01%	24.01%	24.01%	24.01%	24.01%	24.01%
N2	0.61%	0.61%	0.61%	0.61%	0.61%	0.61%	0.61%
02	1.61%	1.61%	1.61%	1.61%	1.61%	1.51%	
S	0.00857%	0.00857%	0.00657%	0.00657%	0.00657%	0.00657%	
Fuel Suffur Content (grains/100 standard cubic feet)	2.00			2.00			
Duct Burner Emissions			100.000				2.470.000
Duct Burner NOx, IbAMBtu (HHV)	0.080	0.080		0.080	0.080		
Duct Burner CO, Ib/MBtu (HHV) Duct Burner UHC (as CH4), Ib/MBtu (HHV)	0.040	0.040		0.040			0.040
Duct Burner VOC (as CH4), IsMBtu (HHV)	0.004	0.004		0.004	0.004		
Duct Burner PM10, Ib/MBtu (HHV) (front half catch only)	0 010	0.010	0.010	0.010	0.010	0.010	0.010
Duct Burner PM10, fb/MBtu (HHV) (front and back half catch)	0.024	0.024	0.024	0.024	0.024	0.024	0.024
American COO anidation rate in Paret Branch swift.	10.00						
Assumed SO2 oxidation rate in Duct Burner, vol% Total SO2, but from Duct Burner Fuel only (effer SO2 oxidation)	10.0%	10.0%		10.0%	10.0%		
Total SO3, but from Duct Burner Fuel only (ener SO2 addition) Total SO3, but from Duct Burner Fuel only (efter SO2 addition)	0.000			0.000			
· · · · · · · · · · · · · · · · · · ·						L	
DB NOx, Ib/n	0.00						
DB CO, to/h	000	0.00		0.00			
	0.00	0.00		0.00			
DB UHC (as CH4), (b/h							
DB VOC (es CH4), fb/h	0.00	0.00		0.00			
DB VOC (as CH4), Ib/h DB PM10, Ib/h (front half catch only)		0.00	0.00	0.00	0,00	0.00	0.00
DB VOC (es CH4), fb/h	0.00 0.00		0.00		0,00	0.00	0.00

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Treasure Coast Energy Center Unit 1							
Black & Ventch Project 138859.0030					l		
1x1 Emissions Estimates							
Case Number	8	9	10	11	12	13	14
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type	Distillate	Natural Gas	Distillate	Natural Ges	Distilitate	Naturai Gas	Distillate
CTG Load	100%	100%	100%	100%	100%	75%	75%
CTG Inlet Air Cooling	Evap. Cooler	OH	Off	Evap. Cooler	Evap. Cooler	Off	Off
CTG Steam/Water Injection	Water	No	Water	No	Water	No	Water
Ambient Temperature, F	100	26	26	73	/3	100	100
HRSG Duct Fring	Unfired 566.31	Unfired 200	Unfired 566.31	Unfired 200	Unfired 566.31	Unfired 2.00	Unfired
Fuel Suffur Content (grains/100 standard cubic feet)	300.31	2.00	500.311	2.00	560.31	2.00]	566.31
Stack Emissions							
Stack Exhaust Analysis - Volume Basis - West	2554 200000 ABOUR	Department	TOWNS COLUMN	S-3757484+ <b>53056</b> 4	786420000700000000000000000000000000000000	888,804,74797,805,03	C. 12 (2) (10) (10) (10)
Ar	0.87%	0.94%	0.89%	0.92%	0.88%	0.91%	0.88%
CO2	5.24%	3.71%	5.24%	3.69%	5,26%	3.66%	5.23%
H2O	13.72%	7.65%	11.49%	9.46%	12.90%	10.14%	12.58%
N2	69.45%	74.85%	71.18%	73.42%	70,10%	72.86%	70,10%
02	10.72%	12.86%	11.19%	12.50%	10.87%	12.43%	10.91%
SO2 (after SO2 cooldation)	0.000020%	0.000090%	0.000020%	0.000090%	0.000020%	0.000090%	0.000020%
SO3 (after SO2 coddation)	0.000010%	0.000040%	0.000010%	0.000040%	0.000010%	0.000040%	0.000010%
Total	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%
	ļ						
Stack Exit Temperature, F	266	179	263	182	265	173	250
Stack Diameter, ft (estimated)	18	18	18	18	18	18	18
Stack Flow, Ibrh	3,482,999	3,633,996	4,003,999 896,229	3,505,997	3,650,999	2,687,998	2,784,999
Stack Flow, sofm	785,997 1,096,306	851,787	1,245,911	784,175 969,409	821,475 1,145,806	603,008 733,824	526,625
Stack Flow, actm Stack Exit Velocity, ft/s	72.0	1,046,682 69.0	82.0	63.0	1,145,800 75.0	733,624	856,388 56.0
SMON EDIT VEROCKY, IUS	72.0	69.0	- 525	03.0	/3.0	40.01	30.0
Stack NOx Empassions without the Effects of Selective Catefully Restaction (SCR)				200	CONTRACTOR OF THE PARTY.	9.000	
NOx, ppmvd (dry, 15% OZ)	42.0	9.0	42.0	9.0	420	9.0	
NOx, ppmvd (dry)	50.0	10.6	58.5	10.8	59.7	10.8	42.0 59.3
NOx, ppmvw (wet)	51.8	9.8		9.8	52.0	9.7	51.7
NOx, to/h as NO2 (includes correction adder)	300.0	62.0		57.0	315.0	43.0	236.0
NOx, th/MBtu (LHV) as NO2 (incl. duct burner fuel)	0.1781	0.0366	0.1782	0.0367	0,1783	0.0364	0.1761
NOx, to/M8tu (HHV) as NO2 (inct. duct burner fuel)	0.1672	0.0330	0.1673	0.0331	0.1674	0.0328	0.1654
Stack NOx Emissions with the Effects of Selective Cetalytic Reduction (SCR)	3.60	(C)	CONTRACTOR S	200 CAN (400 M)	F-77-27-20-20-20-27-19	204	
NOx, ppmvd (dry, 15% O2)	8.0	2.0	8.0	2.0	B.O	2.0	B.0
NCx, ppmvd (dry)	11.4	2.4		24		2.4	11.3
NOx, ppmvw (wel)	9,9	2.2	9.9	2.2		2.1	9.8
NOx, lb/h as NO2 (includes NOx margin applied to CTG)	57.1	13.8		12.7	60.0	9.6	45.0
NOx, Ib/MBtu (LHV) as NO2 (incl. duct burner luel)	0.0339	0.0081	0.0339	0.0082	0.0340	0.0081	0.0336
NOx, Ib/MBtu (HHV) as NO2 (incl. duct burner fuel)	0,0318	0.0073	0.0319	0.0074	0.0319	0.0073	0.0315
COD ANCO also assemble day 4504 COD	<del> </del>		<del></del>				
SCR NH3 stip, pprmvd (dry, 15% O2) SCR NH3 stip, fb/h	5.0	10.0 25.0		10.0	5.0 13.7	10.0 17.4	5.0
OUT REST SEP, LETT	13.1	25.0	14.9	229	13.7	17.4	10,4
Stack CO Entissions	108400 pc. 100 400 400			7 Table 1		British Salator Salat	
	140	7.6	14.4	7.5	14.1		
CO, ppmvd (dry, 15% O2)	20.0	90		90	20.0	7.5	14.2 20.0
CO, ppmwd (dry) CO, ppmw (wet)	17.3	83	17.7	9.0 A1	17.4	9.U B.1	17.4
CO, Ib/h (includes CO margin applied to CTG)	60.1	31.4		28.3		22.0	49.0
CO, Ib/MBtu (LHV) (incl. duct burner fuel)	0.0357	0,0185		0.0182		0.0186	0.0366
CO, Ib/MBtu (HHV) (incl. duct burner fuel)	0.0335	0.0167	0.0344	0.0164		0.0168	0.0343
Stack SO2 Enteriors, after SO2 Oxidation	Maria Albania Andrewson	2010/2019 (#89 <b>2</b> 000000)	Programme Commence	<b>经现在的</b> 人。1995年	717 January 1880	1004-00-00 XX 44-6-00-00-00-00-00-00-00-00-00-00-00-00-0	TO LENGISLATO PO ANTON
	0.0%	0.0%	0.0%	0.0%	0.09	0.0%	0,0%
Assumed SO2 oxidation rate in CO Catalyst, vol%				3.0%	3.0%	3.0%	3.0%
Assumed SO2 coolation rate in CO Catalyst, vors.  Assumed SO2 coolation rate in SCR, vors.	3.0%	3.0%	3.0 %				
	3.0%	3.0%					
Assumed SO2 oxidation rate in SCR, volf6 SO2, pprmet (dny, 15% O2)	3.0%	0.79	0.20	0.79		0.79	0.20
Assumed SO2 oxidation rate in SCR, voffs  SO2, pprmd (dny, 15% O2) SO2, pprmd (dny)	0.20 0.28	0.79 0.94	0.20	0.79	0.28	0.95	0.26
Assumed SO2 oxidation rate in SCR, vol's  SO2, pprmet (dny, 15% O2)  SO2, pprmet (dny)  SO2, pprmet (dny)	3.0% 0.20 0.28 0.24	0.79 0.94 0.86	0.20 0.27 0.24	0.79 0.96 0.86	0.28 0.24	0.95 0.85	0.28 0.24
Assumed SO2 oxidation rate in SCR, volfs  SO2, permet (dny, 15% O2)  SO2, permet (dny)  SO2, permet (dny)  SO2, permet (exet)  SO2, bth	3.0% 0.20 0.28 0.24 1.93	0.79 0.94 0.86 7.45	0.20 0.27 0.24 2.20	0.79 0.95 0.86 6.84	0.28 0.24 2.02	0.95 0.85 5.20	0.26 0.24 1.53
Assumed SO2 oxidation rate in SCR, vol*6  SO2, pprmd (dry, 15% O2)  SO2, pprmd (dry)  SO2, pprmd (dry)	3.0% 0.20 0.28 0.24	0.79 0.94 0.86	0.20 0.27 0.24 2.20 0.0011	0.79 0.96 0.86	0.28 0.24 2.02 0.0011	0.95 0.85	0.20 0.25 0.24 1.53 0.0011 0.0011

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Treasure Coast Energy Center Unit 1							
Black & Ventch Project 138859.0030							
1x1 Emissions Estimates					i		
Casa Number	8	9	10	11	12	13	14
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7
CTG Fuel Type	Distillate	Naturai Gas	Distillate	Natural Gas	Distillate	Natural Gas	Distil
CTG Load	100%	100%	100%	100%	100%	75%	
CTG intel Air Cooling	Evero, Cooler	Off	orr	Every, Cooler	Evan Cooler	Off	
CTG Strem/Water Injection	Water	No	Water	No.	Water	No.	w
Ambient Temperature, F	100		26	73	73	100	••
HRSG Duct Firing	Unfired	Unfired	Unfired	Unfired	Unfired	Unfired	Uni
Fuel Sulfur Content (grains/100 standard cubic feet)	586.31	2.00	566.31	2.00	566.31	2.00	56
	G.C. 31	1.00	330.51		300,51	2.00	
Stack Emissions - continued							
Stack UNC Emissions	\$5,302364V-07346834	84 800 000000	SASA PARAMETERA PA	4/88-23-37-74-88-98		\$200 P\$C \$60000.00	
UHC, pprivid (dry, 15% O2)	5.7	5.4	5.7	6.4	5.7	6.5	
UHC, ppmed	8.1	7.6	7.9	7.7	6.0	7.8	
UHC, pomww	7.0	7.0	7.0	7.0	7.0	7.0	
UHC, Ibrh as CH4 (includes correction adder)	140	15.1	16.0	140	15.0	11.0	
UHC, Ib/MStu (LHV) (Incl. duct burner fuel)	0.0083	0.0089	0.0083	0.0090	0.0065	0.0093	0.0
UHC, loAdStu (HHV) (Incl. duct burner fuel)	0.0078	0.0081	0.0078	0.0081	0.0080	0.0084	0.0
OCIO, PERMONO (CICTO) SIRM, WAS MAKINI 1969	0.0076	0.0001	V.W/8	0.0001	0.0080	0.0004	0.0
	1000		72.675.000.000.000		al Lathin / Spannamic agencia		
Stack VOC Emissions				10. 10.000	2473 3000 0000	E ICHEROTO III MIMINGITI OLE IM	AND THE PROPERTY OF
VOC, ppmvd (dry, 15% O2)	2.8	1.3	2.8	1,3	2.8	1.3	
VOC, ppmvd (dny)	4.1	1.5	4.0	1.5	4.0	1.6	
VOC, ppmvw (wet)	3.5	1.4	3.5	1.4	3.5	1.4	
VOC, lb/h as CH4 (includes VOC correction as applied to CTG)	7.0		8.0	2.8	7.5	2.2	
VOC, Ib/MBtu (LHV) (incl. duct burner fuel)	0.0042	0.0018	0.0042	0.0018	0.0042	0.0019	0.
VOC, Ib/MBtu (HHV) (Incl. duct burner fuel)	0.0039	0.0016	0.0039	0.0018	0.0040	0.0017	D.
PM 10 without the Effects of SC2 unitation	1100 MACAN AND AND	120000000000000000000000000000000000000	**************************************	NAME OF TAXABLE PARTY.	BARBOY 302803-760	\$002954034,505088	Water Control
PM10 Emissions - Front Helf Catch Only							
PM10. Ib/n	17.0	9.0	17.0	9.0	17.0	9.0	
	0.0101	0.0053	0,0089	0.0058			0
PM10, fb/M8tu (LHV) (incl. duct burner fuel)					0.0096	0.0076	
PM10, lb/MBtu (HHV) (Incl. duct burner fuel)	0.0095	0.0048	0.0083	0.0052	0.0090	0.0069	0.
PM10 Emistions - Front and Back Half Catch PM10 Ibh	340	18.0	340	18.0	34.0	180	
PM10, Ib/M8tu (LHV) (incl. duct burner fuel)	0.0202		0.0177	0.0116	0.0192	0.0152	D.
PM10, Ib/MBtu (HHV) (Incl. duct burner fuel)	0.0189		0.0168	0.0104	0.0181	0.0137	0.
PM10 with the Effects of 602 Oxidation (includes (NH4)2-(604)]	0.0000000000000000000000000000000000000	#2000 AMERICA	<b>金沙湖市 1980年1990</b> 年	30 (200) (200)	2500,047 (000,000,000	COMPANY FOR	65.25 (1956×41
PM10 Emissions - Front Half Catch Only	ļ						
PM10, Ib/h	17.0	9.0	17.0	9.0	17.0	9.0	
PM10, tb/MBtu (LHV) (incl. duct burner fuel)	0.0101	0.0053	0.0089	0.0058	0.0098	0.0076	0
PM10, Ib/MBtu (HHV) (Incl. duct burner fuel)	0.0095	0.0048	0.0083	0.0052	0.0090	0.0069	
PM10 Emissions - Front and Back Haff Catch			_				
PM(10, lb/h	35.7	24.6	36.0	24.1	35.8	22.6	
PM10, Ib/MBtu (LHV) (incl. duct burner fuel)	0.0212	0.0146	0.0187	0.0155	0.0203	0.0192	
PM10, Ib/MBtu (HHV) (Incl. duct burner fuel)	0.0199		0.0178	0.0140	0.0190	0.0173	
Total Effects of SC2 Oxidation	THE STATE OF THE S	XX 100 FT NAMES OF	-10"(2011)	9875/500actoris/500/60-	300 March 1886	50000000000000000000000000000000000000	8075636367447,1
Total SO2 to SO3 conversion rate, %vol	30.2%		30.2%	30.2%	30.2%	30.2%	
Total Amount of SO2 converted to SO3. Byth	0.63		0.95	295	0.87	225	
Maximum Stack Ammonium Sulfate [(NH4)2-(SO4)] (assuming 100% convension from SO3), forh	1.72		1.96	6.09	1.80	4.54	-
Maximum Stack H2SO4 (assuming 100% conversion from SO3 to H2SO4), (b/h	1.27		1.45	4.52	1,34	3.44	i
Machinery States (1250-4) (2500) East (100-4) Conversion Holl (250-5) In (250-4); East	1.21	120	1.50	1	1.35	3.00	
Post Combustion Emissions Control Equipment							
Selective Catalytic Reduction (SCR)		1	0.26.74">10.00.88466		2012-2013-000-000		100000000000000000000000000000000000000
NOx Removed in SCR, %wt	81.0%			77.8%	81.0%	77.8%	<b></b>
NOx removed in SCR, Ib/h	242.9		276.9	44.3	255.0	33.4	1
Ammonia Siip, Brh	13.1	25.0	14.9	22.9	13.7	17.4	-
8'	<del></del>	<u> </u>	<del>1</del>		1	<del>                                     </del>	t
s; 1. The emissions estimates shown in the table above are per stack.						I	
						I	
2. The dry of composition used is 0.98% Ar, 78.03% N2 and 20.99% O2							
<ol> <li>Standard conditions are defined as 60 F, 14,696 psia, Norm conditions are defined as 0 C, 1.103 bar</li> </ol>						I	
4. All ppm values are based on CH4 calibration gas.						1	
5. The CTG performance is from GTP, a General Flectric estimation program						I	
The CTG performance is from GTP, a General Electric essention program.     The H2O increase in the SCR catalyst is negligible and not included in the analysis.						1	
The HZO increase in the SCR catalyst is negligible and not included in the analysis.     The VOC/UHC ratio is assumed to be 20% for NG and 50% for distribute.							
						I	
						1	
<ol> <li>Ammonium suffates created downstream of the SCR are included in the back half particulates. The assumption that 100%</li> <li>SON is conserted in arrangement states results in Negral case" particulate emissions.</li> </ol>							
SO3 is converted to ammonium suffates results in "worst case" particulate emissions.							
SO3 is converted to emmonium suffates results in "worst case" perticulate emissions.  9. Where manufacturer data of birk of pollutars emissions were available, the greater of the manufacturer's estimate and B&Va.							
SO3 is converted to ammonium suffates results in "worst case" particulate emissions.							

The front half catch of CT particulate emissions is assumed to be half the emount of the front and back half catch.
 As requested the SCR was designed to reduce the MOx stack emissions to 2 and 6 ppmvd@15%O2 when firing NG and Distillate, respectively.
 The emissions estimate is based on FGT pas with a maximum suffur content of 2.0 grains/100act.

The company count and in the company of the company	Г	1/14/2006							
Column	Л	FMPA							
Columb   C		Black A Vestch Project 132859.0030							
Class	┍		15	16	17	16	19	20 1	21
City and part   City and par	L								
CTO Secretor injects    Total									
Company   Comp		CTG Load							50%
March Complement									
Miles for Free   Control	ı		76 26						26
### And Constant  ### From Property 2.  ### 1997  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 1998  ### 19		HRSG Duct Firing							
Temporary   Temp	H	Fuel Sulfur Content (gratns/100 stendard cubic feet)	2.00	568.31	2.00)	568.311	2.00	566.31)	2.00
Processed proc		Ambient Conditions							
Processed proc	F	Applied Personal at E	20.0	20.0	72.0	73.0	100.0	100	25.0
Constants Telement Processors	Ŀ								
Column   C	Ę	Almospheric Pressure, psia	14.690	14 690	14.690	14,690	14.690	14.690	14.690
Column   C	-	Combustion Turbine Performence							
Column	L		·						
CTO   Company and Pro-Ath French Prince   1985   26   20   20   20   20   20   20   20	$\vdash$	CTG Performance Reference	GTP						
CFC Compare Name Names   1,000									
March 1970	H								
Process   Proc	L								
Column   C	F								
Bear CTS OMES, MY   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1500   1	H	Corpus cust, El. 1720	10.7			10.1	5.2		
Section   Sect	F								
Contract (Contract (Cont	$\vdash$	GROSS CTG COUPUT, RW	137,800			128,700	72,300		
CTI   March	F								
CT12 WARRING STREET AND   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,	$\vdash$	GIDSS CITE Heef Keth, BRUNKWIN (HHV)	10,993	11,438	11,537	11,811	14,432	14,420	13,201
Column   C									
Pennin Park Info   10   12   2   2   10   10   10   10	$\vdash$	CTG Heat input, MBtu/h (HHV)	1,512.7	1,839.1	1,401.7	1,520.1	1,043.4	1,116.2	1,211.8
CT10 - Fermion   Temporary	E								
CTS Companies from March 1971   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.00	H	Injection Fluid/Fuel Ratio	0.0	1.3	0.0	1.2	0.0	1.0	0.0
Test Color for the Am									
Test Circle from Pach	F	CTG Exhaust Temperature, F	1,136	1,136	1,173	1,172	1,200	1,200	1,190
CTD far for regentles	8	Compussion Turbine Foet	N T. Land Married William	PRESENTATION EXTEN	36 76 3 3 5 5 5 6 4 5 6 4 5 6 4 5 6 4 5 6 6 4 5 6 6 4 5 6 6 4 5 6 6 4 5 6 6 4 5 6 6 4 5 6 6 6 6	COMMON STATEMENT	ALTERNATION CONTRACT	STORY BARNE	
Colorative Character Colorative Character Colorative Character Colorative Character Colorative Character	F								
CT   Shelled Answering Proteoms below 1997   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00   19-00	┢	CTG Fuel Temperature, F	380	_60	380		365	60	300
1100   1000   1100   1000   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100   1100									
CTG_Past Companion (Villende Analysis In Vinde)	. H								
## 1	ŀ	<u></u>							
Companies (Prince) Bins: **TRIPS   100-05   177-79   69.09   177-79   69.09   177-79   69.09   177-79   69.09   177-79   69.09   177-79   69.09   177-79   69.09   177-79   69.09   177-79   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   69.09   6	7 ├-		0.00%	0.00%	0.00%	0.00%	0.00%	0.00%	0.00%
10	_								
1811   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975   1975	<u> </u>		73.76%	85.00%	73.76%	85,00%	73.76%		73.76%
Total	F	н2	73.76% 24.01%	85.00% 14.80%	73.76% 24.01%	85,00% 14.60%	73.76% 24.01%	14 80%	73.76% 24.01%
Foot activate Control (general code field)		H2 H2 O2	73.76% 24.01% 0.61% 1.61%	85,00% 14,80% 0,20% 0,00%	73.76% 24.01% 0.61% 1.61%	85.00% 14.80% 0.20% 0.00%	73.76% 24.01% 0.61% 1.61%	14 80% 0.20% 0.00%	73.76% 24.01% 0.61% 1.61%
## CTO Schedule Absorbet Private Besis - Weig   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989		H2 N2 O2 S	73.76% 24.01% 0.61% 1.61% 0.00657%	85.00% 14.80% 0.20% 0.00% 0.00150%	73.76% 24.01% 0.61% 1.61% 0.00657%	85.00% 14.80% 0.20% 0.00% 0.00150%	73.76% 24.01% 0.61% 1.61% 0.00657%	14 80% 0.20% 0.00% 0.00150%	73.76% 24.01% 0.61% 1.61% 0.00657%
## CTO Schedule Absorbet Private Besis - Weig   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989   989		H2 H2 O2 S Total	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00%	85.00% 14.80% 0.20% 0.00% 0.00150% 100.00%	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00%	85,00% 14,60% 0,20% 0,00% 0,00150% 100,00%	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00%	14 80% 0.20% 0.00% 0.00150% 100.00%	73,76% 24,01% 0,61% 1,61% 0,00657%
Ar		H2 N2 O2 S Total Fuel Suther Content (grains/100 standard cubic feet)	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00%	85.00% 14.80% 0.20% 0.00% 0.00150% 100.00%	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00%	85,00% 14,60% 0,20% 0,00% 0,00150% 100,00%	73.76% 24.01% 0.81% 1.61% 0.00557% 100.00%	14 80% 0.20% 0.00% 0.00150% 100.00%	73,76% 24,01% 0,61% 1,61% 0,00657% 100,00%
CO2		H2 H2 Q2 S Total Fuel Sulfur Content (grains/100 standard cubic feet) Complusation Turbine Exhaussi	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00%	85.00% 14.80% 0.20% 0.00% 0.00150% 100.00%	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00%	85.00% 14.80% 0.20% 0.00% 0.00150% 100.00% 586.31	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00	14 80% 0.20% 0.00% 0.00% 100.00% 566.31	73,76% 24,01% 0,61% 1,61% 0,00657% 100,00%
FOC   7.79%   11.67%   2.27%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.72%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%   7.22%	***************************************	H2 H2 O2 S Total Fuel Suther Content (grains/100 abandard cubic feet) Compustion Turbine Exhausi	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00	85,00% 14,80% 0,20% 0,00150% 100,00% 506,31	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00	85.00% 14.00% 0.20% 0.00150% 100.00% 566.31	73,76% 24.01% 0.61% 1.61% 0.00557% 100.00%	14 80% 0.20% 0.00% 0.00150% 100.00% 566.31	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00)
12 pm   10 pm   12 pm   10 pm   12 p		H2 N2 O2 S Total Fuel Suffur Content (grains/100 standard cubic feet) Combussion Turbine Eshauss CTO Exhaust Analysis (Yolune Basis - Wet)	73.76% 24.01% 0.61% 1.61% 1.00% 100.00% 2.00	85.00% 14.80% 0.20% 0.00% 100.00% 566.31	73 78% 24 01% 0 61% 1.61% 0 00657% 100.00% 2 00	85.00% 14.80% 0.20% 0.00% 0.00150% 100.00% 568.31	73.76% 24.01% 0.61% 1.61% 0.0057% 100.00% 2.00	14 80% 0.20% 0.00% 0.00150% 100.00% 566.31	73.78% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00)
SO2, jathe 502 positions   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0.0000794   0	***************************************	H2 H2 H2 O2 S Total Fuel Suther Content (grains/100 standard cubic feet)  Combussion Turbine Exhauss  CTG Eichaust Analysis (Yokuna Basis - Wet)  Ar CO2 H2O	73.76% 24.01% 0.61% 1.61% 0.00857% 100.00% 2.00  0.94% 3.76% 7.76%	85.00% 14.80% 0.20% 0.00% 0.00150% 100.00% 506.31	73 789 24 01% 0.61% 1.61% 0.0057% 100.00% 2.00	85.00% 14.80% 0.20% 0.00150% 100.00% 566.31	73.76% 24.01% 0.61% 0.61% 0.00557% 100.00% 2.00  2.00  0.92% 3.44% 9.73%	14 80% 0.20% 0.00% 0.00150% 100.00% 566.31	73.78% 24.01% 0.61% 1.61% 1.00% 10.00% 2.00)
Total   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   100,0%   10		H2 N2 O2 S Total Fivet Suther Content (grains/100) standard cubic feet) Complication Turbine Exhauss  CTO Eidynigt Analysis (Yolugne Basis - Wel) Ar CO2 H2O N2	73.76% 24.01% 24.01% 0.61% 1.61% 0.00567% 100.00% 2.00  0.94% 3.76% 7.79% 74.79%	85.00% 14.80% 0.20% 0.00% 0.00150% 100.00% 566.31 0.80% 5.44% 11.40% 71.27%	73.76% 24.01% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00  0.52% 3.71% 9.30% 73.51%	85.00% 14.80% 0.20% 0.00150% 100.00% 566.31 0.80% 5.33% 12.40% 70.44%	73.76% 24.01% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00  0.92% 3.44% 9.73% 73.02%	14 80% 0.20% 0.00% 0.00150% 100.00% 566.31 0.99% 4.88% 11.68% 70.89%	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00)
No. ppmd (dr) 19% OD   100   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510   510		N2 N2 O2 S Total Fuel Suffur Content (grains/100 standard cubic feet)  Combussion Turbine Eshauss  CTG Exhaust Analysis (Volume Basis - Wet) Ar CO2 N2 O2 SO2 (after SO2 coldation)	73.76% 24.01% 24.01% 0.01% 1.01% 0.00657% 100.00% 2.00  0.94% 3.76% 7.79% 74.79% 12.65% 0.00010%	85.00% 14.80% 0.20% 0.00% 0.005% 100.00% 596.31 2.80% 5.46% 11.40% 71.27% 10.0003%	73.76% 24.01% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00  0.92% 3.71% 9.30% 73.51% 12.50% 0.00010%	85.00% 14.90% 0.20% 0.00% 100.00% 596.31 0.28% 5.33% 12.45% 70.44% 0.00033%	73.76% 24.01% 0.01% 1.61% 0.00557% 100.00% 2.00  2.00  3.44% 9.73% 73.02% 12.80% 0.00005%	14 80% 0.20% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00%	73.76% 24.01% 2.61% 1.61% 0.00657% 100.00% 2.00) 2.00 2.00 2.00 2.00 2.00 2.00 2.0
Specific Volume (1970)   41.9   41.30   42.31   42.00   41.55	3	H2 H2 H2 H2 O2 S Total Fuel Suthur Content (grains/100 standard cubic feet)  Compussion Turbine Exhaust  CTG Ethougt Analysis (Yolugne Basis - Wet) A A CCC H2O N2 O2 SO2 (after SO2 exidation) SO3 (after SO2 exidation)	73.76% 24.01% 0.61% 1.61% 0.00567% 100.00% 2.00  0.94% 3.76% 7.79% 14.79% 0.00010%	85.00% 14.80% 0.20% 0.00% 100,00% 596.31 2,00% 5.00% 11.60% 71.27% 0.00001%	73.76% 24.01% 0.61% 1.61% 0.00557% 100.00% 2.00  0.92% 3.71% 9.30% 73.51% 0.00002%	85.00% 11.80% 0.22% 0.00% 0.00150% 100.00% 556.31  0.85% 5.33% 12.65% 0.000001%	73.76% 24.01% 0.61% 1.61% 1.00% 100.00% 200 200 200 200 200 200 200 200 200	14 80% 0.20% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00%	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00) 0.94% 3.70% 7.44% 7.465% 0.000012%
Specific Volume, scrib   13.33   13.42   13.47   13.45   13.45   13.45   13.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.25   12.	3	H2 H2 H2 H2 O2 S Total Fuel Sulfur Content (grains/100 standard cubic feet)  Combustion Turbine Exhaust  CTO Ethaust Ansayrids (Yokupe Basis - Wet) A CC2 H2O N2 O2 SO2, (after SO2 coldation) SO3, (after SO2 coldation) Total	73.76% 24.01% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00  0.94% 3.76% 7.76% 7.47% 12.69% 0.00010%	85.00% 14.80% 0.20% 0.00% 0.00150% 100.00% 596.31  2.89% 5.44% 11.45% 71.27% 0.00003% 0.00003% 0.00003%	73.76% 24.01% 24.01% 0.61% 1.61% 0.00557% 100.00% 2.00  0.52% 3.71% 9.30% 73.51% 12.50% 0.00010% 0.00002% 100.00%	85.00% 114.80% 0.22% 0.00% 0.00150% 100.00% 586.31  2.85% 5.33% 12.45% 0.00033% 0.000015%	73.76% 24.01% 24.01% 0.61% 1.61% 0.00557% 100.00% 2.00  0.92% 3.44% 9.73% 73.02% 12.60% 0.00009% 100.00%	14 80% 0.20% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00%	73.76% 24.01% 0.81% 1.61% 0.00557% 100.00% 2.00)  0.94% 3.70% 7.44% 12.87% 0.00010% 0.00002%
Extrausal Class Plans, sciffs  CTG ROS Entistations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internations (Without Prior Controlation Striktstons Control)  Additional Prior of Internation (Without Prior Controlation Striktstons Control)  Additional Prior of Internation (Without Prior Controlation Striktstons Control)  Additional Prior of Internation (Without Prior Controlation Striktstons Control)  Additional Prior of Internation (Without Prior Controlation Striktstons Control)  Additional Prior of Internation (Without Prior Controlation Striktstons Control)  Additional Prior of Internation (Without Prior Controlation Striktstons Control)  Additional Prior of Internation (Without	***************************************	H2 N2 O2 S Total Fuel Suther Content (grains/100 standard cubic feet)  Combustion Turbine Exhauss  CTG Exhaust Analysis (Yokuma Basta - Wet) Ar CD2 H2O N2 O2 SO2, (after SO2 oxidation) SO3, (after SO2 oxidation) Total	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00  2.00  0.94% 3.76% 7.79% 12.69% 0.00010% 0.000007%	85.00% 14.80% 0.20% 0.00% 0.00% 100.00% 506.31	73.76% 24.01% 24.01% 0.61% 1.01% 0.00% 1.00% 2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00	85.00% 114.90% 0.20% 0.00% 0.00150% 100.00% 566.31  2.85% 1.12.40% 10.50% 0.00001% 10.00001% 10.00001%	73.76% 24.01% 0.01% 0.01% 0.00% 1.01% 0.00657% 100.00% 2.00 2.00 2.00 2.00 2.00 2.00 2.0	14 69% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00%	73.76% 24.01% 0.81% 1.61% 0.00% 1.00% 2.00 2.00 2.00 2.00 2.00 2.00 2.00
Additional Princet Marries included in mass based HOT Emissions below 0% 0% 0% 0% 0% 0% 0% 0% 0% 0% 0% 0% 0%	\$	H2 N2 O2 S Total Fuel Suther Content (grains/100 standard cubic feet)  Compusation Turbine Exhausa  CTO Exhausat Analysis (Volume Basis - Well)  Ar CO2 H2O N2 O2 SO2 (after SO2 axidation) SO3 (after SO2 axidation) Total	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00	85.00% 14.80% 0.20% 0.00% 0.00% 100.00% 506.31  77 20% 100.00% 54.6% 11.46% 10.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00%	73.76% 24.01% 0.61% 1.01% 0.00% 1.00% 1.00% 2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  3.11% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 3.10% 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Additional Percent Margin included in mass based (NDE Emissions below   0%   0%   0%   0%   0%   0%   0%   0	***************************************	H2 N2 O2 S Total Fuel Suthur Content (grains 100 standard cubic feet) Combustion Turbine Exhauss  CTO Exhaust Analysis (Volume Basis - Wet) Ar Ar CO2 H2O N2 O2 SO2, (after SO2 caldation) SO3, (after SO2 caldation) Total  Motecular WI, Evinol Specific Volume, B**3/b	73.76% 24.01% 24.01% 0.01% 1.01% 0.00657% 100.00% 200  0.94% 3.76% 7.79% 74.79% 0.00010% 0.00000% 100.00% 13.33 2.012.955	85.00% 14.80% 0.20% 0.00% 0.00150% 100.00% 596.31  2.89% 5.46% 71.27% 10.0003% 0.00003% 100.00001% 100.000 22.20 40.12 13.42 2.088,186	73.76% 24.01% 24.01% 0.61% 1.61% 0.00567% 100.00% 2.00  0.92% 3.71% 9.30% 73.51% 12.50% 0.00010% 100.00% 1100.00% 1101.00%	85.00% 14.90% 0.20% 0.00% 0.00150% 100.00% 596.31  0.88% 5.33% 12.45% 70.44% 10.05% 100.00% 100.003% 100.00% 110.00%	73.76% 24.01% 24.01% 0.81% 1.65% 1.00557% 100.00% 2.00 2.00 2.00 2.00 2.00 2.00 2.0	14 89% 0 0001% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 100000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 10000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 10000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 10000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 10000000% 1000000% 1000000% 1000000% 1000000% 1000000% 1000000% 10000000% 1000000% 1000000% 1000000% 1000000% 10000000% 10000000% 10000000% 10000000% 10000000% 100000000	73,76% 24,01% 24,01% 0,81% 1,61% 0,00657% 100,00% 2,00)  2,00)  3,70% 7,84% 74,65% 12,57% 0,00010% 0,00022% 100,0% 41,56 13,33 1,717,254
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H2 N2 O2 S Total Fuel Suthur Content (grains 100 standard cubic feet) Combustion Turbine Exhauss  CTO Exhaust Analysis (Volume Basis - Wet) Ar Ar CO2 H2O O2 SO2, (after SO2 caldation) SO3, (after SO2 caldation) Total  Motecular WI, Evinol Specific Volume, Br3tb Specific Volume, Brath Exhaust Gas Flow, scrim	73.76% 24.01% 24.01% 0.01% 1.01% 0.00657% 100.00% 2.00  0.94% 3.76% 7.75% 12.65% 0.00010% 0.000003% 100.00% 100.00% 20.40% 100.00% 100.00% 20.40% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 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NOL permet (day)  NOL permet (day)  10.00  50.00  10.00  50.00  10.00  50.00  10.00  50.00  10.00  50.00  10.00  50.00  10.00  50.00  10.00  50.00  10.00  50.00  10.00  50.00  10.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  50.00  5		H2 H3 Total Fuel Sulfur Content (grains/100 standard cubic feet)  Combustion Turbine Exhaust  CTO Eichaugt Anstyrids (Yolugne Basis - Well)  Ar Ar H2 H3	73.76% 24.01% 24.01% 1.61% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.00% 1.0	85.00% 14.80% 1.20% 0.20% 0.00% 0.00150% 100.00% 596.31  2.00% 5.44% 11.40% 71.27% 0.00003% 0.00003% 0.00003% 100.00% 28.22 13.42 2.088,186 691,801	73.78% 24.01% 24.01% 0.61% 1.61% 0.000% 100.00% 200  0.92% 3.71% 9.90% 73.51% 10.000% 10.0002% 10.0002% 110.00% 24.139 13.42 14.19 13.42 1,851.720 535.884	85.00% 114.90% 0.20% 0.00050% 100.00% 556.31  0.88% 5.33% 12.40% 10.50% 10.00% 10.00% 10.00% 11.00%	73.76% 2401% 2401% 0.61% 1.61% 0.0057% 100.00% 2.00 2.00 2.00 2.00 2.00 2.00 2.0	14 89% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.0000% 0.00	73.78% 24.01% 0.81% 1.61% 0.00557% 100.00% 2.00)  0.94% 3.70% 7.64% 7.46% 112.67% 0.00010% 0.00002% 110.00% 28.47 41.50 13.33 1,717.254
NO., pormer (left)   1000		H2 H	73.76% 24.01% 24.01% 0.01% 1.01% 0.00657% 100.00% 2.00  0.04% 3.76% 7.79% 7.479% 12.66% 100.0003% 100.00% 2.00  2.00  2.00  0.00003% 100.00% 2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.00  2.0	85.00% 14.80% 10.20% 0.00% 0.00150% 100.00% 596.31  2.00% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 1.1.40% 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NOx, But 8 NO2		H2 N2 N2 S Total Fuel Sulfur Content (grains/100 standard cubic feet)  Computation Turbine Ethauss  CTO Ethaust Analysis (Volume Basis - Well) Ar Ar Ar CC2 N2 N2 N2 N2 N3 SO2 (after SO2 addation) SO3 (after SO2 addation) Total  Motecuter WI, Evinor Specific Volume, Ar3th Specific Volume, act70 Ethaust Gas Flow, actm Ethaust Gas Flow, actm Ethaust Gas Flow, actm  CTO NOT Enrichtors (Without Post Combustion Entistions Control)  CTO ROT Enrichtors (Without Post Combustion Entistions Control)  CTO ROT Enrichtors (Without Post Combustion Entistions Control)  Nox, pormet (dry, 15% O2)	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00  0.94% 3.76% 74.79% 112.69% 0.00010% 0.00010% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 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NO., BANBRU (19HV)  CTG CD Entrisistems (Without Post Combustion Entrisions Control)  Additional Procent Margin included in mass bessed CD Entrisistons below  ON.  ON.  ON.  ON.  ON.  ON.  ON.  ON		H2 N2 N2 S Total Fuel Suthar Content (grains 100 standard cubic feet) Combustion Turbine Exhauss  CTO Exhaust Anseynis (Volume Basis - Wet) Ar Ar C02 H20 N2 S02, (after S02 coldation) S03, (after S02 coldation) S03, (after S02 coldation) Total  Motecular VI, formol Specific Volume, ar3/b Notational Proceet Margin included in mass beaset NOx Emissions Control Additional Proceet Margin included in mass beaset NOx Emissions Control NOx, pprend (dry, 15% O2) NOx, pprend (dry, 15% O2)	73.76% 24.01% 24.01% 0.01% 0.0057% 100.00% 100.00% 2.00  0.94% 3.76% 7.75% 12.65% 0.00010% 0.00003% 100.00% 100.0% 25.46% 5.72.469  0% 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 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CTG CD Enrissistems (Mithout Pear Combustion Enrissions Control)   CO. permet (Mary) included in mass based CD Emissions below		H2 N2 N2 S Total Fuel Sulfur Content (grains 100 standard cubic firet) Combustion Turbine Exhauss  CTO Exhaust Analysis (Violume Basis - Wet) Ar Ar C02 H20 N2 S02, (after S02 coldation) S03, (after S02 coldation) Total  Motecular WI, Evinol Specific Volume, Br3/b Specific Vo	73.76% 73.76% 74.01% 0.61% 0.00657% 100.00% 100.00% 2.00  0.94% 3.76% 7.76% 11.26% 0.00010% 0.00003% 100.0% 3.900 10.00 0% 9.000 10.00 0% 9.000 10.00 0% 9.000 10.00 0% 9.000 10.00 0% 9.000 10.00 0% 9.000 10.00 9.000 10.000 9.000	85.00% 14.80% 0.20% 0.000% 0.00150% 100.00% 596.31  2.08% 1.40% 1.40% 0.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 1.00000% 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Additional Percent Margin included in mass based CO Emissions below  ON  ON  ON  ON  ON  ON  ON  ON  ON  O		H2 N2 N2 S Total Fuel Suths Content (grains/100 standard cubic feet) Combustion Turbine Exhaust  CTO Eidhaust Anathysis (Yolugne Basis - Wed) A A CC02 H20 N2 O2 SO2 (after SO2 oxidation) SO3, (after SO2 oxidation) Total Mosecular WI, Ehrnol Specific Volume, in 3th Specific Volume, in 3th Specific Volume, in 3th Specific Volume, in 3th Specific Volume, act/b Exhaust Gas Flow, actim Exhaust Gas Flow, actim Company Gas Flow, actim Additional Percent Margin included in mass besed NOx Emissions Control NOx, ppmed (dry), 15% O2) NOx, ppmed (dry) NOx, bit is in NO2 NOx b	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00  0.04% 3.76% 74.76% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 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CO, ppmel (dry, 15% O2)  CO, ppmel (dry)  SOZ, p		H2 N2 N2 S Total Fuel Suths Content (grains/100 standard cubic feet) Combustion Turbine Exhaust  CTO Eidhaust Analysis (Yolugne Basis - Welt) A A CC02 H20 N2 O2 SO2 (after SO2 oxidation) SO3, (after SO2 oxidation) Total Mosecular WI, Ehrnol Specific Volume, in 3/th Specific Volume, in 3/th Specific Volume, in 3/th Specific Volume, act/b Exhaust Gas Flow, actim Exhaust Gas Flow, actim Additional Percent Margin included in mass besed NOx Emissions Control Additional Percent Margin included in mass besed NOx Emissions Control NOx, pomed (dry, 15% O2) NOx, pomed (dry) NOx, both as NO2 NOx, both as NO2 NOx, both BNO2 NOx, both BN D(2) NOX BN D(2) NOX BN D(2) NOX BN	73.76% 24.01% 0.61% 1.01% 0.00657% 100.00% 2.00  0.04% 3.76% 74.76% 74.76% 0.00010% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 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CO. ppried (dry)  CO. ppried (dry)  8.30  17.70  8.20  17.50  8.30  17.70  8.20  17.50  8.10  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17.70  8.30  17		H2 N2 O2 S Total Fuel Sulfur Content (grains/100 standard cubic feet)  Computation Turbine Ethauss  CTO Exhaust Analysis (Volume Basis - Well) Ar Ar CO 1470 N2 O2 SO2 (after SO2 addation) SO3 (after SO2 addation) Total  Molecular WI, Brimol Specific Volume, act70 Ethaust Gas Flow, scfm  Echaust Gas Flow, scfm  CTO NOX Enrissions (Without Post Combustion Enrissions Control) NOX, pomel (etv.) 15% O2) NOX, permel (etv.) NOX, brims NOZ NOX Drimspanner (british Nox British Nox Bri	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00  0.94% 3.76% 74.79% 74.79% 112.69% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 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CO, ppmw (wet)   8.30   17.70   8.20   17.50   8.10   17.70   8.20   17.50   8.10   17.70   8.20   17.50   8.10   17.70   8.20   17.50   8.10   17.70   8.20   17.50   18.4   41.1   20.33   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   20.00   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20.00   20.00   20.00   20.00   20.00   20.00		H2 N2 O2 S Total Fuel Suthur Content (grains/100 standard cubic feet)  Computation Turbine Exhauss  CTG Exhaust Analysis (Yoluppe Basis - Wed) Ar Ar CCC H2O N2 O2 SO2 (after SO2 exidation) SO3 (after SO2 exidation) SO3 (after SO2 exidation) Total  Metecular W/I, Ehrned Specific Volume, sh'3th Specific Volume, sh'3th Specific Volume, sciff Exhaust Gas Flow, sciff Exhaust Gas Flow, sciff Exhaust Gas Flow, sciff Content of the Son of the S	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00  0.94% 3.76% 74.79% 74.79% 112.69% 0.00010% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 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Additional Percent Margin included in Inh SQZ Emissions Delive		H2 N2 N2 S Total Fuel Sulfur Content (grains/100 standard cubic firet) Combustion Turbine Exhaust  CTO Eichaugt Anishysis (Yohapie Besis - Wel) A A CC CQ H2 Q2 SQ2 (after SQ2 coldation) SQ3 (after SQ2 coldation) SQ3 (after SQ2 coldation) SQ3 (after SQ2 coldation) Total Melecular WI, Romal Specific Volume, n°3/b Specific Volume, n°3/b Specific Volume, act/b Exhaust Gas Flow, act/m Exhaust Gas Flow, act/m Exhaust Gas Flow, act/m Content of the Sqr Flow, act/m Synchic Volume, act/b Content of the Sqr Flow, act/m Additional Percent Margin included in mass bessed CO Emissions below Content of the Sqr Flow, act/m Additional Percent Margin included in mass bessed CO Emissions below Content of the Sqr Flow, act/m Additional Percent Margin included in mass bessed CO Emissions below Content of the Sqr Flow, act/m Additional Percent Margin included in mass bessed CO Emissions below Content of the Sqr Flow, act/m Additional Percent Margin included in mass bessed CO Emissions below Content of the Sqr Flow, act/m Additional Percent Margin included in mass bessed CO Emissions below Content of the Sqr Flow, act/m C	73.76% 24.01% 061% 101% 0.0065% 100.00% 2.00  0.04% 3.76% 74.76% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 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Evinol Specific Volume, Art 3th Specific Volume, act 3th Ethaust Gas Flow, scrim Ethaust Gas Flow, scrim Crass Gas Flow, scrim Crass Gas Flow, scrim Additional Percent Margin included in mass based NOx Emissions Control) NOx, permed (dry, 15% O2) NOx, permed (dry) NOx, behalbu (LHV) NOx, behalbu (LHV) NOx, behalbu (LHV) NOx, behalbu (LHV) NOx, permed (dry) NOX, permed (	73.76% 73.76% 74.01% 0.61% 1.61% 0.0057% 100.00% 2.00  0.04% 3.76% 7.76% 7.76% 12.65% 100.00% 10.000 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 10.00 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Assumed SO2 axidation rate in CTG, veRs 20 9s 20	***	H2 N2 N2 S Total Fuel Suthur Content (grains/100 standard cubic feet)  Complusation Turbine Exhauss  CTG Exhaust Analysis (Yolugne Basis - Wed) Ar Ar CCC H2O N2 N2 N2 N2 N3 SO3 (after SO2 exidation) SO3 (after SO2 exidation) SO3 (after SO2 exidation) Total  Metecular WI, Ehrod Specific Volume, sh'8b Specific Volume, sciff Exhaust Gas Flow, sciff Exhaust Gas Flow, sciff Exhaust Gas Flow, sciff Nonumer Son, sciff Nonumer Margin included in mass based NOx Emissions Control) NOx, permet (sty) NOx, permet (sty) NOx, permet (sty) NOx, both as NO2 NOx, both as NO3 NOX	73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00  0.94% 3.76% 7.76% 74.79% 112.69% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 0.00010% 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SOZ, ppmwl (dry)         1.0951         0.3252         1.0922         0.3221         1.0170         0.2924         1.0702           SOZ, ppmwl (wel)         1.0997         0.2978         0.9899         0.2919         0.9911         0.9911         0.2582         0.9865           SOZ, Bbh         5.900         2.0165         5.3748         1.8700         4.7459         1.3732         5.51148           SOZ, bMRBu (LHV)         0.0050         0.0013         0.0050         0.0013         0.0050         0.0013         0.0050         0.0013         0.0050	***	H2 N2 N2 S Total Fuel Suths Content (grains/100 standard cubic firet)  Combustion Turbine Exhaust  CTG Exhaust Analysis (Yoluspe Basis - Wet) A A CCC H2 N2 N2 N2 N2 N2 SO2 (after SO2 exidation) SO3 (after SO2 exidation) Total Missech Wil, thrind Specific Volume, n°17b Specific Volume, n°17b Specific Volume, n°17b Specific Volume, sc/7b Exhaust Gas Flow, sc/m Exhaust Gas Flow, sc/m Additional Percent Margin included in mass beset NOx Emissions Control) NOx, permet (dry 15% O2) NOx, permet (dry) NOx, permet (dry) NOx, beth as NO2 NOx, bM8bu (HYV)  CTG OD Emissions (Without Post Combustion Emissions Control)  C (D, ppmet (dry) NOx, bM8bu (HYV)  CTG OD Emissions (Mithout Post Combustion Emissions Control) C (D, ppmet (dry) NOx bM8bu (HYV)  C (D, ppmet (dry) C (D, ppmet (vert) C (D, ppmet (vert) C (D, ppmet (dry) C (D, ppmet (vert) C (D, ppme	73.76% 24.01% 0.61% 0.0057% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 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SOZ, ppmwl (dry)         1.0951         0.3252         1.0922         0.3221         1.0170         0.2924         1.0702           SOZ, ppmwl (wel)         1.0997         0.2978         0.9899         0.2919         0.9911         0.9911         0.2582         0.9865           SOZ, Bbh         5.900         2.0165         5.3748         1.8700         4.7459         1.3732         5.51148           SOZ, bMRBu (LHV)         0.0050         0.0013         0.0050         0.0013         0.0050         0.0013         0.0050         0.0013         0.0050	***	H2 N2 N2 S Total Fuel Suths Content (grains/100 standard cubic firet)  Combustion Turbine Exhaust  CTG Exhaust Analysis (Yoluspe Basis - Wet) A A CCC H2 N2 N2 N2 N2 N2 SO2 (after SO2 exidation) SO3 (after SO2 exidation) Total Missech Wil, thrind Specific Volume, n°17b Specific Volume, n°17b Specific Volume, n°17b Specific Volume, sc/7b Exhaust Gas Flow, sc/m Exhaust Gas Flow, sc/m Additional Percent Margin included in mass beset NOx Emissions Control) NOx, permet (dry 15% O2) NOx, permet (dry) NOx, permet (dry) NOx, beth as NO2 NOx, bM8bu (HYV)  CTG OD Emissions (Without Post Combustion Emissions Control)  C (D, ppmet (dry) NOx, bM8bu (HYV)  CTG OD Emissions (Mithout Post Combustion Emissions Control) C (D, ppmet (dry) NOx bM8bu (HYV)  C (D, ppmet (dry) C (D, ppmet (vert) C (D, ppmet (vert) C (D, ppmet (dry) C (D, ppmet (vert) C (D, ppme	73.76% 24.01% 061% 1.61% 0.00657% 100.00% 2.00  0.04% 3.76% 7.76% 12.65% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 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SO2, bMBu (LHV) 0.0050 0.0013 0.0050 0.0013 0.0050 0.0013 0.0050	***	H2 N2 N2 S Total Fuel Sulfur Content (grains/100 attandand cubic firet) Combustion Turbine Ethaust  CTO Ethaust Ansayrids (Yokape Basis - Wed) A A CC2 H2 Q2 Q2 Q3 SO2, (after SO2 coldation) SO3, (after SO2 coldation) SO3, (after SO2 coldation) So30, (after SO2 coldation) Total Melecular WI, formal Specific Volume, n°3/b	73.76% 73.76% 24.01% 0.61% 0.00657% 100.00% 2.00  0.00657% 100.00% 2.00  0.0067% 0.0001% 0.0001% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 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SO2, IAM/8th (HHV) 0.0045 0.0012 0.0045 0.0012 0.0045 0.0012 0.0045	***	H2 N2 N2 S Total Fuel Suths Content (grains/100 standard cubic firet) Combustion Turbine Exhaust  CTG Ethoust Analysis (Yoluspe Basis - Wet) A A A CCC H2 O2 N2 O2 SO2 (after SO2 exidation) SO3 (after SO2 exidation) Total  Mescular MA, brind Specific Volume, n°2/b Exhaust Gas Flow, scfib Exhaust Gas Flow, scfib Exhaust Gas Flow, scfib Additional Percent Margin included in mass based NOx Emissions Control NOx, permet (dry) NOx, permet (dry) NOx, permet (dry) NOx, permet (dry) NOx, brins NO2 NOx, brins NO2 CO, pprind (dry) NOx, brins NO2 CO, pprind (dry) CO, pprin	73.76% 73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00  0.00657% 100.00% 2.00  0.00657% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 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	***	H2 N2 N2 S Total Fuel Suths Content (grains/100 standard cubic firet)  Combustion Turbine Exhaust  CTG Etheust Analysis (Yoluspe Basis - Wet) A A CCC H2 N2 N2 O2 SO2, (after SO2 exidation) SO3, (after SO2 exidation) Total Mescular MA, brind Specific Volume, n°1/b Specific Volume, n°1/b Specific Volume, act/b Exhaust Gas Plow, actm Exhaust Gas Plow, actm Exhaust Gas Plow, actm Additional Percent Margin included in mass beset NOx Emissions Control) NOx, permed (dry, 15% O2) NOx, permed (dry) NOx, permed (dry) NOx, brins NO2 NOx, brins NO2 NOx, brins NO2 CO, pprind (dry, 15% O2) SO2, pprind (dry) SO2, brints (drift) SO3, brints (drift) SO4, brints (drift) SO3, brints (drift) SO4, brints (drift) SO4, brints (drift) SO5, brints (drift) SO5, brints (drift) SO5, brints	73.76% 73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00  0.00657% 100.00% 2.00  0.00104 3.76% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 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	***	H2 N2 N2 S Total Fuel Suths Content (grains/100 standard cubic firet)  Combustion Turbine Exhaust  CTG Etheust Analysis (Yoluspe Basis - Wet) A A CCC H2 N2 N2 O2 SO2, (after SO2 exidation) SO3, (after SO2 exidation) Total Mescular MA, brind Specific Volume, n°1/b Specific Volume, n°1/b Specific Volume, act/b Exhaust Gas Plow, actm Exhaust Gas Plow, actm Exhaust Gas Plow, actm Additional Percent Margin included in mass beset NOx Emissions Control) NOx, permed (dry, 15% O2) NOx, permed (dry) NOx, permed (dry) NOx, brins NO2 NOx, brins NO2 NOx, brins NO2 CO, pprind (dry, 15% O2) SO2, pprind (dry) SO2, brints (drift) SO3, brints (drift) SO4, brints (drift) SO3, brints (drift) SO4, brints (drift) SO4, brints (drift) SO5, brints (drift) SO5, brints (drift) SO5, brints	73.76% 73.76% 24.01% 0.61% 1.61% 0.00657% 100.00% 2.00  0.00657% 100.00% 2.00  0.00104 3.76% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 100.00% 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1.61% 0.0057% 100.00% 200 200 200 200 200 200 200 200 200	14 80% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 0.00% 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Case N  CTG M  CTG FI  CTG LI  CTG LI  CTG LI  CTG SI  Ambient  HRSG  Fuel St  Combo  Addition  UHC,	bodel  set 7 ypa  set Af Coding  basan/Wilser Injection  If emperature, F  Duct Firing  filtur Content (grain/a) (00 standard cubic feet)  settion Turbine Exhaust - continued  PIC Entistions (Without Post Combustion Entissions Control) (10 Standard Coding Content Margin Inducted in Bih UHC Emissions Below  permed (day, 15% O2)	PG7241 Natural Gas 75% Off No 28 Unified 200	PG7241 Distillate 75% Off Water 25 Undred \$66.31	17 PG7241 Natural Gas. 75% Off No 73 Unfred 2,00	18 PG7241 Distribute 75% Off Water 73 Unfired 566.31	19 PG7241: Natural Ges 50% Off No 100 Unfred 2.00	20 PG7241 Distillate 50% Off Water 100 Unifred 566.31	PG7241 Natural Gas SON Off No 26 Unfined
CTG FI CTG LI CTG LI CTG SI Ambien HRSG Fuel SI  Comba  Comba  UHC, UHC, UHC, UHC, UHC, UHC, UHC,	uel Typa  and  tet Af Coding  bear Af Coding	Netural Ges 75% Off No 26 Unified 200	Distillate 75%, Off Water 26 Unfred 566.31	Naturai Gas 75% Off No 73 Unfired	Distillate 75% Off Water 73 Unfired	Natural Ges 50% Off No 100 Unfired	Distillate 50% Off Water 100 Unfired	Natural Gas. 50% Off No 26
CTG LC CTG II CTG SI Ambient HRSG Fuel Su Combs Addit UHC, UHC, UHC, UHC, UHC, UHC, UHC, UHC,	and  Int Air Cooling  It ampressure, F  Duct Firing  Situr Content (gravins/100 standard cubic feet)  isstion Turbline Enhaust - continued  Interpressure (Without Post Combustion Emissions Control)  Interpressure (Without Post Combustion Emissions Control)  Interpressure (Without Post Combustion Emissions Below  John Percent Margin included in 8th UHC Emissions Below  John (dry, 15% OZ)	75% Off No 26 United 2.00	75% Off Water 26 Unfined 566.31	75% Off No 73 Unfired	75% Off Water 73 Unfired	50% Off No 100 Unfired	50% Off Water 100 Unfired	50% Off No 26
CTG SI Ambien HRSG Fuel Su Combs SSREE CTG U Addu UHC, UHC, UHC, UHC, UHC, UHC, UHC,	Item/Whiter Injection It Presperature, F Duct Fring Strut Content (grains/100 standard cubic feet) usstion Turbine Exhaust - continued HC Emissions (Withbout Post Combustion Enfantons Control) Form Presert Marph Inducted in Ibih UHC Emissions Below permed (dny, 15% OZ)	No 26 Unitred 2.00	Water 26 Untired 566.31	No 73 Unfired	Water 73 Unfired	No 100 Unfred	Water 100 Unfired	No 26
Ambien HRSG Fuel Su  Combs  OTA U  Addit  UHC, UHC, UHC, UHC, UHC, UHC, UHC, UHC	It Temperature, F Duck Fring Under Fring U	26 Unfired 2.00	26 Unfired 566.31	73 Unfired	73 Unfired	100 Unfired	100 Unfired	26
Fuel Su Comba Comb	action Turbine Exhaust - continued  HC Emissions (Without Post Combustion Emissions Control)  And Percent Margin included in bith UHC Emissions Below  permed (dy, 15% OZ)	2.00	566.31					Unfired
Comba  Addition  UHC.  UHC.  UHC.  UHC.	astion Turbine Exhausi - continued  HC Emissions (Without Post Combustion Emissions Control) 보스 경우병에 중에 독표한 구독수는 전쟁을 하는 , top Percent Marpin included in 5th UHC Emissions Below permed (dry, 15% OZ)		x **P\$					200
UHC, UHC, UHC, UHC, UHC	pomed (dry, 15% O2) permed (dry)		12 X 72 X ACRESON C 2021 (9)					
UHC, UHC, UHC, UHC, UHC,	ppmvd (dry, 15% O2) ppmvd (dry)	0.04	0.0%	0.0%	0.0%	0.0%	0.0%	0.0%
UHC, UHC	, ppm/vd (dry)							
UHC UHC		6.3 7.6	5.5 7.9	6.4 7.7	5.6 8.0	6.9 7.8	6.1 7.9	6.4 7.6
UHC	ppmww (wet)	7.0	7.0	7.0	7.0	7.0	7.0	7.0
UHC	, b/n as CH4	12.0	123	11.3	12.0	9.1	9.3	10.0
	, IDMBIU 25 CH4 (LHV)	0.0088	0.0080 0.0075	0.0089	0.0064 0.0079	0.0096 0.0067	0.0069	0.0092 0.0083
SWEETEN V	OC Biresstons (Without Post Combustion Emissions Control)	***************************************	UNITED STORES NO		ZONEN CAZNASIG	#1500 Prints Co. 101975		
	OL pressions (region) Fost Consulation pressions below	0%	0%	0%	0%	0%	0%	0%
voc	percentage of UHC	20%	50%	20%	50%	20%	50%	20%
voc	, pprivd (dry, 15% O2)	1.3	2.7	1.3	2.8	1.4	3.0	1.3
	, porrivid (dry)	1.5	4.0 3.5	1.5 1.4	4.0 3.5	1,6	4.0	1.5
	, ppmw (wet) , b/h as CH4	2.4	5.5 6.1	2.3	5.5	1.4	3.5 4.7	2.0
VOC	, Ib/MBtu es CH4 (LHV)	0.0018	0.0040	0.0018	0.0042	0.0019	0.0044	0.0018
VOC	, Io/MBtu as CH4 (HHV)	0.0016	0.0037	0.0016	0.0039	0.0017	0.0042	0.0017
	M10 Emissions (without the Effects of SO2 Oxidation)	0%	0% CONTRACTOR	0%	0%	0%	0%	0%
	Emissions - Front Half Catch Only							
	O, Exh	9.0	17.0	9.0	17.0	9.0	17.0	9.0
	O, Ib/MBtu (LHV)	0.0086	0.0110	0.0071 0.0064	0.0119	0.0096	0.0162	0.0082
PM10	O, Io/MBtu (HHV)	0.0059	0.0104	0,0084	0.0112	0,0086	0.0152	0.0074
	Emissions - Front and Back Haff Catch							
	0, Ib/h	18.0 0.0132	34.0 0.0221	18.0 0.0142	34.0 0.0238	18.0 0.0191	34.0 0.0324	18 0 0.0165
	O, IDMABIL (HHY)	0.0119	0.0207	0.0128	0.0224	0.0173	0.0305	0.0149
HRSO	Duct Burners							
Durel F	Signed Puel		Service Committee			77 <b>8</b> 74	21 70 V 100 V 10 P	(1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00 (1.00
Duct B	turner Heat Input, MBtu/h (LHV)	0.0	0.0	0.0	0.0	0.0	0.0	0.0
	turner Heat Input, MBtu/h (HHV)  Duct Burner Fuel Flow, Itv/h	0.0	0.0	0.0	0.0 D	0.0	0.0	0.0
	turner Fuel LHV, Btwtb	20,816	20,816	20,616	20,816	20,816	20,816	20,816
Duct B	Jurner Fuel HHV, Btu/fb	23,091	23,091	23,091	23,091	23,091	23,091	23,091
Duct B	Surner Fuel Composition (Ultimate Analysis by Weight)							
Ar C		0.00% 73.76%	0.00%	0.00% 73.76%	0.00% 73.76%	0,00% 73.76%	0.00% 73.76%	0.00% 73.76%
H2		24.01%	24.01%	24.01%	24.01%	24.01%	24.01%	24.01%
N2		0.61%		0.61%	0.61%	0.61%	0.61%	0.61%
02 S	<del>-</del>	1.61% 0.00657%		1.61% 0.00657%	1.61% 0.00657%	1.61%	1.61% 0.00857%	1.61% 0.00857%
Total		100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%
	sulfur Content (grains/100 standard cubic feet)	2.00	2.00	2.00	2.00	2.00	2.00	2.00
	Surmer Emissions		SHIPS SAME SHARE	ASSESSA NA CONTRACTOR	745-60-00	- Transferre	100000000000000000000000000000000000000	718.00 ( C C C C C C C C C C C C C C C C C C
	Surner NOx, IbMBN (HHV)	0.080	0.060	0.060	0.080	0.080	0.080	0.080
	Surner CO, Ib/MBtu (HHV) Surner UHC (as CH4), Ib/MBtu (HHV)	0.040	0.060	0.040	0.040	0.040	0.040	0.040
Duct B	Surner VOC (as CH4), Ib/MBtu (HHV)	0.004	0.004	0.004	0.004	0.004	0.004	0.004
	Surner PM10, Ib/MBtu (HHV) (front half catch only) Surner PM10, Ib/MBtu (HHV) (front and back half catch)	0.010 0.024		0.010 0.024	0.010 0.024	0.010	0.010	0.010
							0.024	0.024
	ned SO2 coldation rate in Duct Burner, vol's	10,0%		10.0%	10.0%	10.0%	10.0%	10.09
	SO2, Ib/h from Duct Burner Fuel only (after SO2 addation) SO3, Ib/h from Duct Burner Fuel only (after SO2 addation)	0.000		0.000	0.000	0.000	0.000	0.000
L								
	NOX, Buth	0.00		0.00	0.00	0.00	0.00	0.00
	UHC (as CH4), Ib/h	0.00		0.00	0.00	0.00	0.00	0.00
DB \	VOC (as CH4), lb/h	0.00	0.00	0.00	0,00	0.00	0.00	0.00
	PM10_lbh (front haif catch only)	0.00		0.00	0.00			0.00
UB	PM10, lbh (front and back half catch)	0.00	0.00	3.00	0.00		0.00	0.00

1/14/2006 FMPA							
Trassure Coast Energy Center Unit 1							
Black & Vestch Project 138859.0030							
1x1 Emissions Estimates							
Case Number	15	15	17	18	19	20	21
		~				L "	•
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type	Natural Gas	Distillate	Natural Gas	Distillate	Natural Gas	Distitate	Natural Gas
CTG Load	75%	75%	75%	75%	50%	50%	50%
CTG Intel Air Cooling	Off	Off	Off	Off	Off	Off	Off
CTG Starm/Water Injection	No	Water	No	Water	No	Water	No
Ambient Temperature, F	26	26	73	73	100		26
HRSG Duct Fring	Unfred	Unfired	Unfired	Unfired	Unfired	Unfired	Linfired
Fuel Suthur Content (grains/100 standard cubic feet)	2.00	568.31	2.00	568.31	2.00	566.31	2.00
Stack Emissions							
Stack Exhaust Analysis - Vokane Basis - Wet	令·众·张本治的(300)	是在在上級自然關係	2007/06/90/9000-70	<b>新型公司服务的</b>	<b>2.10美智的20多位的30</b>	District Control	THE PERSON OF THE
Ar	0.94%	0.89%	0.92%	0.88%	0.92%		0.94%
CO2	3.78%	5.44%	3.71%	5.33%	3.44%	4.88%	3,70%
H2O	7.79%	11.49%	9.36%	12.49%	9.73%	11.68%	7.64%
N2	74.79%	71.27%	73.51%	70.44%	73.02%	70.89%	74.85%
02	12.59%	10.90%	12.50%	10.85%	12.89%	11.65%	12.87%
SO2 (after SO2 oxidation)	0.000090%	0.000030%	0.000090%	0.000020%	0.000080%	0.000020%	0.000090%
SO3 (after SO2 oxidation)	0.000040%	0.000010%	0.000040%	0.000010%	0.000030%	0,000010%	0.000040%
Total	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%
Stack Edit Temperature, F	167	247	172	248	167	243	158
Stack Diameter, ft (estimated)	18	18	18	18	187	18	18
Stack Flow, Ib/h	3,026,997	3,092,999	2,842,997	2,915,999	2,276,998	2,340,999	2,477,998
Stack Flow, acfm	572,499	5,032,399	635,884	654,642	510,428	524,774	550,529
Stack Flow, actin	811,236	941,303	772,822	891,810	615,929	709,713	654,192
Stack Exit Velocity, ft/s	53.0	62.0	51.0	58.0	40.0		43.0
Company and							
Stack NOs Emissions without the Effects of Selective Catalytic Reduction (SCR)	machine microsa	A COMPANY OF STREET	0.00		57500000000000000	Secretary (1967)	ACT NO LESS TO THE
NOx, ppmed (dry, 15% O2)	90	42.0	9.0	420	9.0	42.0	9.0
NOx, ppmvd (dry)	10.9	60.8	10.8	60.2	10.1		10.6
NOx, parnw (wet)	10.0	53.8	9.8	52.7	9.1	48.3	9.8
NOx, bth as NO2 (includes correction adder)	50.0	273.0	46.0	252.0	34.0		39.2
NOx, Ib/MStu (LHV) as NO2 (Incl. duct burner fuel)	0.0367	0.1774	0.0364	0.1798	0.0361	0.1759	0.0369
NOx, bMBtu (HHV) as NO2 (incl. duct burner fuel)	0.0331	0.1668	0.0328	0,1658	0.0326	0.1652	0.0324
Stack NOs Endstions with the Effects of Selective Catalytic Reduction (SCR)	的研究解析的表面的	SALA SE SALAS		Same Title of the Control	SEASSEMENT OF THE	<b>经济资本均约</b>	
NOx, pprintd (day, 15% O2)	2.0	8.0	2.0	8.0	2.0	8.0	20
NOx, pprind (dry)	2.4	11.6	2.4	11.5	22		2.4
NOx, ppmw (wet)	2.2	10.2	22	10.0	2.0		2.2
NOx, both as NO2 (includes NOx margin applied to CTG)	0.0081	52.0 0.0338	10.2 0.0081	48.0 0.0336	7.6 0.0080		8.7
NOx, IbMBtu (LHV) as NO2 (Incl. duct burner fuel) NOx, IbMBtu (HHV) as NO2 (Incl. duct burner fuel)	0.0081	0.0338	0.0081	0.0336	0.0000	0.0335	0.0080
TOWA, SUMBLING (COLOR) 40 NOZ (SEC. QUAL DELINE 1999)	0.0073	0.0317	0.00/3	U.U.318	9.0072	0.0315	0.0072
SCR NH3 stp, pprivd (dry, 15% O2)	10.0	5.0	10.0	50	10.0	5.0	10.0
SCR NH3 stip, Ibh	20.1	11.9	18.7	11,1	13.9	8.1	16.1
			I				ļ .
Stack CO Projectors	0.00019097512000	CONTRACTOR	1275 Marie 1275 July 2012	00.22	Section of the sec	16-2.2 FELL 18-13	357000000000000000000000000000000000000
CO, ppmvd (dry, 15% O2)	7.5	13.8	7.5	14.0	8.0	154	7.6
CO, ppmvd (dry)	9.0	20.0	9.0	200	9.0		90
CO, pprove (wet)	8.3	17.7	8.2	17.5	8,1		B.3
CO, Ib/h (Includes CO margin applied to CTG)	25.0	54.2	23.0	51.0	18.4		20.3
CO, Ib/MBtu (LHV) (incl. duct burner fuel)	0.0183	0.0352	0.0162	0.0357	0.0195	0.0392	0.0186
CO, Ib/MStu (HHV) (incl. duct burner fuel)	0.0165	0.0331	0.0164	0.0336	0.0176	0.0368	0.0167
Stack 802 Emissions, after 802 Oxidation		Distriction of	19878 3 617 (24)	1000	our keid Gersagah		torn was applicable
Assumed SO2 coddation rate in CO Catalyst, vol'%	0.0%	0.0%		0.0%			0.01
Assumed SO2 addition rate in SCR, with	3.0%	3.0%	3.0%	3.0%	3.0%	3.0%	3.09
SO2, porred (dry, 15% O2)	0.79	0.20		0.20			0.7
SO2, ppmvd (dry)	0.96	0.28		0.28	0.89		0.9
SO2, ppriy/w (wet)	0.68	0.25		0.25	0.80		0.8
SO2, Both	6 D1 0,0044	1.78	5,57 0,0044	1,63 0,0011	4.14 0.0044		4.8
SO2, IbMBtu (LHV) (incl. duct burner fuel) SO2, IbMBtu (HHV) (incl. duct burner fuel)	0.0044	0.0011	0.0044	0.0011	0.0044		0.004
I SOA EFROM (DOY) (RC, OCC OUTS (US)	0.0040	0.0011	0.0040	0.0011	3.0040	0.0011	I 0.0040

1/14/2006	
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FMPA
Treasure Coast Energy Center Unit 1
Black & Vestch Project 138859.0030
1x1 Emissions Estimates

Case Number	15	16	17	16	19	20	21
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type	Natural Gas	Otstiffete	Natural Gas	Distillate	Natural Gas	DistiBate	Natural Gas
CTG Load	75%	75%	75%	75%	50%	50%	50%
CTG Intel Air Cooling	Off	OH	Off	Off.	Off	Off	Off
CTG Steam/Water Injection	No	Water	No	Water	No	Water	No
Ambient Temperature, F	26	26	73	73	100	100	26
HRSG Duct Firing	Unfired	Unfired	Unfired	Unfired	Unfired	Unfired	Unfired
Fuel Suffur Content (grains/100 standard cubic feet)	2.00	586.31	2.00	· 586.31	2.00	568.31	2.00

STACE Emissions - continued							
学の Stack UHC Emissions 2009 からできる 2000 A 2	工艺品"等是940年40年	SECTION TO SECTION	Aのでは、2174年の名の金融機構	<b>安全的中心2008</b> 图	A THE TRANSPORTED TO	# : POSSESSON NEWSFORD	WITCH DEPTHENCE VIEW
UHC, pprivd (dry, 15% O2)	6.3	5.5	6,4	5.6	6.9	6.1	6.4
UHC, ppmrd	7.6	7.9	7.7	80	7.8	7.9	7.6
UHC, ppmww	7.0	7.0	7.0	7.0	7.0	7.0	7.0
UHC, forh as CH4 (includes correction adder)	120	12.3	11.3	12.0	9.1	9.3	10.0
UHC, Ib/MBtu (LHV) (incl. duct burner fuel)	0.0088	0.0000	0.0089	0.0084	B900.0	0.0089	0.0092
UHC, Ib/MBtu (HHV) (incl. duct burner fixel)	0.0079	0.0075	0,0081	0.0079	0.0087	0.0084	0.0083
Stack VOC Emissions	17.585	Charles Care	11 11 11 11 11 11 11 11 11 11 11 11 11	NO CALBORITY COLUM	THE REPORT OF THE PARTY OF THE	PR (2002) 126+345	SHIPP A LESSE
VOC, ppmred (dry, 15% O2)	1.3	2.7	1.3	2.8	1.4	3.0	1.3
VOC, ppmvd (dry)	1.5	4.0	1.5	4.0	1.6	4.0	1.5
VOC, ppmww (wet)	1.4	3.5	1.4	3.5	1.4	3.5	1.4
VOC, Ib/h as CH4 (includes VOC correction as applied to CTG)	2.4	8.1	2.3	6.0	1.8	4.7	2.0
VOC, lb/MBtu (LHV) (incl. duct burner fuel)	0.0018	0.0040	0,0018	0.0042	0.0019	0.0044	0.0018
VOC, Ib/MBtu (HHV) (incl. duct burner fuel)	0.0016	0.0037	0.0016	0.0039	0,0017	0.0042	0.0017
PRINTO withhout the Effects of SC2 axidetion	The street of the state of	Figures, Schoolschill	海水科研研開展	W. C. S. C. C. S. C.	ESCOPE A SIGNATURE	/GPetter washing	g satters and the
PM 10 Emissions - Front Haff Catch Only							
PM10, ts/h	9.0	17.0	9.0	17.0	9.0	17.0	9.0
PM10, Ib/MBtu (LHV) (incl. duct burner fuel)	0.0086	0.0110	0.0071	0,0119	0.0096	0.0162	0.0082
PM10, Ib/MBtu (HHV) (incl. duct burner fuel)	0.0059	0.0104	0.0064	0.0112	0.0086	0.0152	0.0074
PM10 Emissions - Front and Back Haff Catch		<b></b>					
PMt0, to/h	18.0	34.0	18.0	34.0	18.0	34.0	18.0
PM10, tb/MBtu (LHV) (incl. duct burner fuel)	0.0132	0.0221	0.0142	0.0238	0.0191	0.0324	0.0165
PM10, Ib/MBtu (HHV) (incl. duct burner fuel)	0.0119	0.0207	0.0128	0.0224	0.0173	0.0305	0.014
PMHS with the Effects of GC2 Oxidation [includes (MHI2-(SC4))	But were the second	<b>网络内外科技术</b> 化酚基磺胺	Description of	THE PROPERTY OF STREET	理ない。存在なな数が対	788 Table 176 Table 178	<b>电影响性性测点处</b>
PM10 Ernissions - Front Half Catch Only				_			
PM10, Ib/h	9.0	17.0	9.0	17.0	9.0	17.0	9.0
PM10, Ib/MBtu (LHV) (incl. duct burner fuel)	0.0066	0.0110	0.0071	0.0119	0.0096	0.0162	0.006
PM10, Ib/M8tu (HHV) (Incl. duct burner fuel)	0.0059	0.0104	0.0064	0.0112	0.0086	0.0152	0.007
PM10 Emissions - Front and Back Half Catch							
PM10, lb/h	23.4	35.6		35.5	21.7	35,1	22:
PM10, Ib/MBtu (LHV) (incl. duct burner fuel)	0.0171	0.0231	0.0182	0.0248	0.0231	0.0336	0.020
PM10, th/MBtu (HHV) (Incl. duct burner fuel)	0.0154	0.0217	0.0164	0.0233	0.0208	0.0314	0.018
Total Effects of SOI Custation	(30)。战略战器战器战器	TO LANGE WELL STATE	<b>交出的基础整理符件</b> 基本	がある。	70000000000000000000000000000000000000	SHEAR PACKAGE	CONTRACTOR MARKET
Total SO2 to SO3 conversion rate, %vol	30.2%	30,2%		30.2%	30.2%	30.2%	30.2
Total Amount of SO2 converted to SO3, Ib/h	2.59	0.76		0.70	1.79	0.52	2.0
Maximum Stack Ammonium Surfate [(NH4)2-(SO4)] (assuming 100% conversion from SO3), both	5.35	1.57	4.96	1.45	3.69	1.07	4.2
Maximum Stack H2SO4 (assuming 100% conversion from SO3 to H2SO4), bth	3.97	1.16	3.68	1.08	2.74	0.79	3,11
			L		I	<u> </u>	

#### Post Combustion Emissions Control Equipment

Selective Catalytic Reduction (SCR)	70 <b>3</b> 45770708000	15-00-27 (1987)	27. Sp. 22.000 (2005)	THE PROPERTY OF THE PARTY OF TH	94 T. C. WOLLDWICK	March Add Appropriation	THE BUTCH
NOx Removed in SCR, %wt	77.8%	81.0%	77.8%	81.0%	77.8%	81.0%	77.8%
NOx removed in SCR, b/h	38.9	221.0	35.8	204.0	26.4	149.2	30,5
Arrmonia Sip, forh	20.1	11.9	18.7	11.1	13.9	8.1	16,1
			1	1			

- The emissions estimates shown in the bible above are per stack,
   The dry air composition used is 0.99% Az, 78.00% N2 and 20.99% O2
   Standard conditions are defined as 60 F, 14,696 pale, Norm conditions are defined as 0 C, 1,103 bar
- A All gorn values are based on CH4 calibration gas.
  The CTG partformance is from GTP, a General Electric estimation program.
  The H2O increase in the SCR catalyst is negligible and not included in the enables.
  The VCOLHIC ratio is assumed to be 20% for NG and 50% for distillate.

- A Ammonfauth sulfitties created downstream of the SCR are included in the back half particulates. The assumption that 100% SO3 is converted to emmonium suffates results in "worst case" particulate emissions.
- 9. Where manufacturer data of bith of politizard emissions were evaluable, the greater of the manufacturer's estimate and B&V's estimates were adjusted, where applicable.
  10. Duct burner emissions are included. The duct burner pollutant emissions are Black & Vestch estimates bessed on low NOx duct burner emissions data (provided by Forusy).
- The front half catch of CT perficulate emissions is assumed to be half the emount of the front and back half catch.
   As requested the SCB was designed to reduce the NOx stack emissions to 2 and 8 providing 15%-02 when firing NG and betablet, resourchely.
   The emissions estimate is based on FGT pas with a materium suffur content of 2.0 prainart 00bcd.

U14/2005 FMPA						- 40	
Treasure Coast Energy Center Unit 1 Black & Vestch Project 138889,0030							
1x1 Emissions Estimates Case Number	22	23	24	45	50	51	52
CTG Model CTG Fuel Type	PG724) Distillate	PG7241 Natural Gas	PG7241 Oistillate	PG7241 Naturai Gas	PG7241 Natural Gas	PG7241 Natural Gas	PG7241 Natural Gas
CTG Land CTG trinst Air Cooling	50% Off	50%	50%	100%	100% Evrap. Cooler	100% Evap, Cooler	100% Off
CTG SteamWater Injection	Water	No	Water	No	No.	No No	No
Ambient Temperature, F HRSG Duct Firing	26 Unfired	73 Unfired	73 Unfired	100 Fired	Fired	Unfired	59 Fired
Fuel Sulfur Content (greins/100 standard cubic feet)	568.31	2.00	568.31	2.00	2.00	2.00	2.00
Ambient Conditions							
Ambient Tempershire, F Ambient Retaine Humidity, %	28 0 100.0	73.0 81.5	73.0 81.5	100.0 48.4	59.0 60.0	59.0 60.0	59.0 60.0
Atmospheric Pressure, pale	14.690	14.690	14.690	14,690	14,690	14,690	14.690
Combustion Turbine Performance							
CTG Performance Reference	GTP	GTP	GTP	GTP	GTP	GTP	GTP
CTG Inlet Air Conditioning Effectiveness, % CTG Compressor Inlet Dry Bufb Temperature, F	0 26.0	0 73.0	0 73.0	0 100.0	85 \$2.6	85 52.6	0 59.0
CTG Compr. Inlet Retative Humidity, %	100.0	81.5	81.6	48.5	92.9	92.9	60.2
Inhet Loss, in. H2O Exhaust Loss, in. H2O	4.0 7.5	4.0 6.7	4.0 7.0	4.0 12.3	4.0 15.3	4.0 15.3	4.0 15.0
					100%		100%
CTG Load Level (percent of Base Load) Gross CTG Output, NW	50% 95,500	50% 81,000	50% 85,800	100% 144,600	172,200	100% 172,200	169,000
Gross CTG Heat Rate, Brufn/Wh (LHV)	12,710	12,450	13,090	9,835	9,355	9,355	9,390
Gross CTG Heat Rate, Btu/kWh (HHV)	13,536	13,811	13,941	10,910	10,377	10,377	10,416
CTG Heat Input, MBtu/h (LHV) CTG Heat Input, MBtu/h (HHV)	1,213.8 1,292.7	1,008.5 1,118.7	1,123.1 1,196.2	1,422.1 1,577.6	1,610.9 1,787.0	1,610.9 1,787.0	1,586.9 1,760.3
CTG Water/Steam Injection Flow, but	75,980	0	63,080	0	0	0	0
Injection Fluid/Fuel Ratio	1.2	0.0	1.0	0.0	0.0	0,0	0.0
CTG Exhaust Flow, Ibrh CTG Exhaust Temperatus, F	2,514,000 1,190	2,363,000 1,200	2,418,000 1,200	3,236,000 1,183	3,546,000 1,110	3,646,000 1,110	3,802,000 1,118
Combustion Turbine Fuel	1,000		,,===			1,110	
Total CTG Fuel Flow, Ib/h	66,330	48,450	61,370	68,320	77,390	77,390	76,240
CTG Fuel Temperature, F	60	365		365	365	365	365
CTG Fuel LHV, Btu/fb CTG Fuel HHV, Btu/fb	18,300 19,490	20,816 23,091	18,300 19,490	20,816 23,091	20,816 23,091	20,816 23,091	20,816 23,091
HHV/LHV Ratio	1.0850	1.1093	1.0650	1.1093	1.1093	1.1093	1,1093
CTG Fuel Composition (Uttimate Analysis by Weight) Ar	0.00%	0.00%	0.00%	0.00%	0.00%	0.00%	0.00%
С H2	85.00% 14.80%	73,76% 24.01%	85.00% 14.80%	73.78% 24.01%	73,76% 24.01%	73.76% 24.01%	73.76% 24.01%
N2 O2	0.20%	0.61%	0.20%	0.61%	0.61% 1.61%	0.61% 1.61%	0.61%
S Total	0,00150%	0.00857% 100.00%	0.00150%	0.00657%	0.00657%	0.00657%	0.00857%
Fuel Suthur Content (grains/100 standard cubic feet)	100.00% 566.31	2.00	566.31	2.00	2.00	2.00	2.00
Combustion Turbine Exhaust							
CTG Exhaust Analysis (Volume Basis - Wet)		20,800		- T - M	744.00	16 2/34(5/34 <b>0</b> )886	7 (X) (A)
	0.90% 5.29%	0.92% 3.56%	0.89% 5.07%	0.91% 3.66%	0.93% 3.70%	0.93% 3.70%	0.93%
H2O	10.69% 71.83%	9.09% 73.62%	11.45% 71.15%	10.14% 72.86%	8.38% 74.27%	8.38% 74.27%	8,15% 74.45%
O2 SO2, (after SO2 axidation)	11.28%	12.81%	11,43% 0.00003%	12.42% 0.00010%	12.72% 0.00010%	12.72% 0.00010%	12,789
SO3, (after SO2 cookdation) Total	0.00001%	0,00002%	0.00001%	0.00002%	0.00002%	0.00002%	0.000029
Molecular VVI, Ib/mol	28.35	28.30	28.24	28.19	28.39	28.39	28.41
Specific Volume, ncfbb Specific Volume, ncfb	41.73 13.38	42.14 13.41	42.19 13.43	, 40.61 13.46	38.92 13.37	38.92 13.37	39.06 13.35
Exhaust Gas Flow, actm	1,748,487	1,659,614 528,131	1,700,257	2,200,339	2,365,039	2,365,039	2,344,902
Exhaust Gas Flow, actm	560,622		541,229	725,718	812,450	812,450	801,445
CTG NOx Britissions (Without Post Combustion Emissions Control)  Additional Percent Margin Included in mass based NOx Emissions below	0%	0%	0%	0%	0%	#13 - 7 1800 - New York	(b) (1) (1) (0) (0) (0) (0) (1) (1) (1) (1) (1) (1) (1) (1) (1) (1
NOx, pprivd (dry, 15% O2)	42.00		42.00	9.00	9.00	9.00	9.00
NOx, ppmvd (dry) NOx, ppmvv (wel)	58.60 52.30		56.60 50.20	10.80 9.70	10.70 9.80	10.70 9.80	10.60 9.80
NOx, bith as NO2 NOx, biM8tu (LHV)	213.5 0.1759	36.2	197.6 0.1759	52.0 0.0366		59.0 0.0368	58.0 0.0365
NOx, Iz/MBtu (HHV)	0.1652		0.1652	0.0330		0.0330	0.0329
CTG CO Emissions (Without Post Combustion Emissions Control)  Additional Percent Margin included in mess based CO Emissions below	\$805857. (J. 1883) \$ 0%	2000 200 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	0%	0%	Y	\$ 70.00 × 2000	(A) 1/4 (A) 1/
							2 87
CO, ppmvd (dry, 15% O2) CO, ppmvd (dry)	14.30 20.00	9.00	14 80 20 00	9.00	7.60 9.00	9.00	7.60 9.00
CO, ppm/w (wet) CO, bth	17.90 45.0	19.1	43.0	8.10 28.0	8.20 30.0		8.30 29.4
CO, In/MBtu (LHV) CO, In/MBtu (HHV)	0.0371 0.0348		0.0383 0.0359	0.0183 0.0185		0.0186 0.0168	0.0185
CTO SO2 Emissions (After SO2 Oxydetion, Without Post Combustion Emissions Control)	e arangen regionale	844.544.(A.4631)(C	TERROL SOCIETIES	2000 <b>00</b> 0000000000000000000000000000000		7 A-5-F4-6 (93 <b>0)</b>	S-12880020460
Additional Percent Margin included in Ibih SO2 Emissions below Assumed SO2 oxidation rate in CTG, vol*\( \)	20.0%	0.0%	0.0%	0.09	0.09	0.0%	0.0° 20.0°
SO2, pprind (dry, 15%, Q2) SO2, pprind (dry)	0.2247 0.3135	1.0463	0.3030	1.0862	1.0782	1.0782	0.9083
SO2, pprinw (wet) SO2, Ibrit	0.2800 1.5904	5.0883	0.2683 1.4715	7.1751	8.1276	8.1278	0.9856 8.0068
SO2, IbMBtu (HIV)	0.0013					0.0050 0.0045	0.0050 0.0045
				<u> </u>		<u> </u>	L

1/14/2006		·					
FMPA							
Yreesure Coest Energy Center Unit 1 Black & Vestch Project 138559,0030							
1x1 Emissions Estimates							
Case Number	22	23	24	45	50	51	52
CTG Model CTG Fuel Type	PG7241	PG7241	PG7241 Distillate	PG7241	PG7241	PG7241	PG7241 Natural Gas
CTG Load	Distillate 50%	Natural Gas 50%	SO%	Natural Gas 100%	Natural Gas 100%	Natural Gas 100%	100%
CTG Intel Air Cooling	Off	Off	Off	Off	Evap, Cooler	Evap, Cooler	Off
CTG Steam/Water Injection	Water	No	Water	No	No	No	No
Ambient Temperature, F	26	73	73	100	59	59	59
HRSG Duct Firing Fuel Suffur Content (grains/100 standard cubic feet)	Unfired 566.31	Unfired 2.00	Unfired 566.31	Fired 2.00	Fired - 2.00	Unfired 2.00	Fired 2.00
FOR SUITE CORES (Easter Cores Inc.)	300.31	2.00	300.31)	2.00	2007	2.001	2.00
Combustion Turbine Exhaust - continued				- 1			
		,,,,,	. ,				
CTG UHC Emissions (Without Post Combustion firmissions Control) (本名は、タファンディストルモントルトル・サイル・サイル	で露落が、世界を含ん		<b>发展的问题和数学数据的</b>		7- E0-009-00045**********************************	を表れる大学が大学である。	
Additional Percent Margin included in Ityh UHC Emissions Below	0.0%	0.0%	0.0%	0.0%	0.0%	0.0%	0.0%
UHC, pprrvd (dry, 15% O2)	5.6	6.7	5,9	6.5	64	6.4	6.4
UHC, pprivid (dry)	7.8	7.7	7.9	7.8	7.6	7.6	7.6
UHC, pprnww (wet)	7.0	7.0	7.0	7.0	7.0	7.0	7.0
UHC, Ibrh as CH4	10.0	9.4	10.0	13.0	14.4	14.4	14.2
UHC, IDMBtu as CH4 (LHV) UHC, IDMBtu as CH4 (HHV)	0.0082	0.0093	0.0089	0.0091	0.0090 0.0081	0.0090	0.0090
	0.0077	0.0004	0.004	0.0002	V 1001	0,0001	
CTG VOC Entessors (Without Post Combustion Entessons Control)	2008/8/2002	The Strain Street	ST. ALIVE WINEFOR	2,4968pt 98475200	E-10/7010/09/2015	1944 C C C C C C C C C C C C C C C C C C	40668 (NO. 2017) (MASS)
Additional percent margin included in fb/h VOC emissions below	0%	0%	0%	0%	0%	0%	0%
VOC necessary of IMC	50%		50-	200		200	
VOC persentage of UHC  VOC, ppmvd (dry, 15% O2)	2.8	20%	50%	20%	20%	20%	20%
VOC, ppmvd (dry)	3.9	1.5	4.0	1.6	1.5	1.5	1.5
VOC, pprowr (wet)	3.5	1.4	3,5	1.4	1.4	1.4	1.4
VOC, buth as CH4	5.0	1.9	5.0	2.6	2.9	29	2.8
VOC, IbMBtu as CH4 (LHV) VOC, IbMBtu as CH4 (HHV)	0.0041	0.0019 0.0017	0.0045	0.0018 0.0016	0.0018	0.0018	0.0018
VCC, LIMBUL SE CITY (FITY)	0.0003	0.0017	0.0042	0.0010	0.0010	0.0010	0.0010
CTQ PM10 Errasations (without the Effects of SOZ Oxidation)	THE PARTY OF THE P		5 × 1 3 × 25 × 25 × 2	等4000年800年4月1日2月1日	CRETO PRODUCTION	Market Commence	
Percent margin included in PM10 emissions below	0%	0%	0%	0%	D%	0%	0%
PM10 Emissions - Front Half Catch Onty PM10, Ibh	17.0	9.0	17.0	9.0	9,0	9.0	9.0
PM10, Ib/MBtu (LHV)	0.0140	0.0089	0.0151	0.0063	0.0058	0,0056	0,0057
PM10, Io/MBtu (HHV)	0.0132	0.0000	0.0142	0.0057	0.0050	0.0050	0.0051
			_			_	
PM10 Emissions - Front and Back Half Catch PM10, Ib/n	34.0	18.0	34.0	18.0	18.0	18.0	18.0
PM10, Ib/MBtu (LHV)	0.0280	0.0178	0.0303	0.0127	0.0112	0.0112	0.0113
PM10, IbMBtu (HHV)	0.0263	0.0161	0.0284	0.0114	0.0101	0.0101	0.0102
	<u></u>	<u> </u>	<u> </u>		V-1_4		
MORA Duel Durana							
HRSG Duct Burners							
Duct Burner Puel	ARTITLE CHEST STATE	Photography with the second second	13000000000000000000000000000000000000	ALESS RESIDENCE PARTY	K College (Constitution)	PERCENT AND AND AND A	147-F-14419880000-4111-0000
Duct Burner Heat Input, MBtu/h (LHV)	0.0	0.0	0.0	509.6	481.9	0.0	487.1
Duct Burner Heel Input, MBtu/h (HHV)	0,0	0.0	0.0	565.3	534,6	0.0	540.3
Total Duct Burner Fuel Flow, byh			-	24,480	23,150		23,400
			_				
Duct Burner Fuel LHV, Btufto	20,816	20,816	20,816	20,816	20,816	20,816	20,816
Duct Burner Fuel HHV, Sturto	23,091	23,091	23,091	23,091	23,091	23,091	23,091
Duct Burner Fuel Composition (Ultimate Analysis by Weight)		-					
Ar	0.00%	0.00%	0.00%	0.00%	0.00%	0.00%	0.00%
C	73.76%	73.76%	73.76%	73.76%	73.76%	73.76%	73.76%
H2	24.01%	24.01%	24.01%	24.01%	24.01%	24.01%	24.01%
N2	0.61%	0.61%	0.61%	0.61% 1.61%	0.61%	0.61%	0.61%
\$	0.00657%	0.00657%	0.00657%	0.00657%	0.00857%	0.00657%	0.00657%
Total	100.0%	100.0%		100,0%	100.0%	100.0%	100.0%
Fuel Suffur Content (grains/100 standard cubic feet)	2.00			2.00	2.00		2.00
	CYCCO THE DIE TONG LIBRORY IN	CYMESTERS COM IN	+4.100402200344************	1 MC to \$150,000,000 (\$10,000,000,000,000)	(Discharge degrees bev. 2000.esc	CAMPAGES ZOOTTONIS ALBORIO DEL	MINOR WARELES
知識性 Duct Burner Emissions (ロンイル 大きない 大きなできる 大きなできる 大きない 大きない 大きない 大きない 大きない 大きない 大きをはない 大きをはない 大きない Duct Burner NOx, ながあない (HHV)	0.080	0.080		0.080	0,080	0.080	0.080
Duct Burner CO, Its/MBtu (HHV)	0.040	0.040		0.040	0.040		0.040
Duct Burner UHC (as CH4), fb/M8tu (HHV)	0.080	0.060	0.060	0.060	0.060	0.060	0.060
Duct Burner VOC (as CH4), IbMBtu (HHV)	0.004	0.004	0.004	0.004	0.004	0.004	0.004
Ouct Burner PM10, Ib/MBtu (HHV) (front helf catch only)  Duct Burner PM10, Ib/MBtu (HHV) (front and beck helf catch)	0.010 0.024	0.010	0.010	0.010 0.024	0.010	0.010	0.010
District Control of the Control of the Control	0.024	0.024	0.024	0.024	0.024	0.024	0.024
	10.0%			10.0%	10.0%	10.0%	10.0%
Assumed SO2 oxidation rate in Duct Burner, vol%		0.000	0.000	2.892	2.735	0.000	2.765
Total SO2, Ib/h from Duct Burner Fuel only (after SO2 exidation)	0.000					0.000	0.384
	0.000		0.000	0.402	0.380	0.000	0.00
Total SO2, bith from Duct Burner Fuel only (after SO2 oxidation)  Total SO3, bith from Duct Burner Fuel only (after SO2 oxidation)	0.000	0.000					
Total SO2, Buth from Duct Burner Fuel only (after SO2 oxidation)  Total SO3, Buth from Duct Burner Fuel only (after SO2 oxidation)  DB NOx, Buth DB CO, Buth	0.000	0.000	0.00	45.20 22.60	42.80 21.40	0.00	43.20
Total SO2, lish from Duct Burner Fuel only (after SO2 addation) Total SO3, lish from Duct Burner Fuel only (after SO2 addation)  DB NOs, lish DB CO, lish DB UHC (as CH4), lish	0.000 0.00 0.00	0.000 0.00 0.00 0.00	0.00	45.20 22.60 33.90	42.80 21.40 32.10	0.00	43.20 21.60 32.40
Total SO2, But from Duct Burner Fuel only (after SO2 oxidation)  Total SO3, But from Duct Burner Fuel only (after SO2 oxidation)  DB NOs, But  DB NOs, But  DB UNC (as CH4), But  DB VOC (as CH4), But	0.000 0.00 0.00 0.00	0.000 0.00 0.00 0.00	0.00 0.00 0.00	45.20 22.60 33.90 2.30	42.80 21.40 32.10 2.10	0.00 0.00 0.00 0.00	43.20 21.60 32.40 2.20
Total SO2, lish from Duct Burner Fuel only (after SO2 addation) Total SO3, lish from Duct Burner Fuel only (after SO2 addation)  DB NOs, lish DB CO, lish DB UHC (as CH4), lish	0.000 0.00 0.00	0.000 0.00 0.00 0.00	0.00 0.00 0.00 0.00	45.20 22.60 33.90	42.80 21.40 32.10	000 000 000 000	43.20 21.60 32.40

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Transact Coard Pump Codes Mail 1 Internal A Vision Program Challed Mail 1 Internal A Vision C	1/14/2006							
Base   Service   Table   Tab								
1.								
Commerce								
Column		72	23	24	-6	50	51	52
CCTO part from CCTO comment of	I				~	~	,	
CTG Load and Long CTG Load and	CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CT 10 per Marche Septimen 1997 1997 1997 1997 1997 1997 1997 199	CTG Fuel Type	Distiliate	Natural Gas	Distillate	Natural Gas	Natural Gas	Natural Gas	Natural Gas
CTG Generators promoted assessment of the control p	CTG Load	50%	50%	50%	100%	100%	100%	100%
Animate Transparin, F   138   77   77   78   78   78   78   78	CTG inlet Air Cooling	Off	Off	Off	Off	Evap. Cooler	Evap. Cooler	Off
MEST CONFERENCE   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,				Water	No	No	No	
First Direct Angle System (1987)   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1,000   1							59	
Back Distance								
See Tennish Name   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   1966   19	Fuel Suffur Content (grains/100 standard cubic feet)	566.31	2.00	566.31	2.00	2.00	2:00	2.00
A 1 99%								
A 1 99%	Stack Exhaust Analysis - Yokune Basis - Wet			YSSELERAL TRUE	9.47.8XX 1883.388	SPLEASE FROM THE	28 CHARGES AND STATES	WHEN SHOUTS AND
1909		0.90%	0.92%	0.89%	0.90%	0.92%	0.93%	0.92%
19.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1.00 1.1								
1								10.23%
SOCI petter SOCI petter SOCI presidency								73.63%
Social Personne   Social Per								
Seed, Edit Temperature,   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00   1907.00								
Sinck Eat Temperature								
Sear Damework   16   18   18   18   18   18   18   18	Total	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%
Sear Damework   16   18   18   18   18   18   18   18	Shah Sa Tamandan S	342	101			<del></del>		
Stack Place Alth								
Stock Pleas achm   Stock Pleas								2675 706
Seco Flow cethin   Seco Flow c								
Sept. NO. general entries of Belletchia Calabytic Reduction (SCR)   Sept.								
Start No. Epression inflinint the Effects of Belechin Gethy (Sp. 194 O)								
Most, permet (dw, 15% O2)					35.0			
MOX, general (de), 15% O2	Start NOz Emissions without the Effects of Selective Catalytic Reduction (SCR)	80000000000000000000000000000000000000	965 50 - TABLES	mariametrican	72,000,000,000	. 30 (4) (1) (4)	SEASON RESERVED.	300000000000000000000000000000000000000
NOx, permet (eth)								12.1
MOx, permer (cett)								18.9
NOL, Britis NOZ (includes contraction adois)		52.3	9.4	50.2		16.8	9.8	17.0
NO., particle (HHV) as NO2 (incl. duct burner bar)		213.5	36.2	197.5	97.2	101.8	59.0	101.2
Size NO: Extension with the Effects of Selective Catalytic Reduction (SCR)								0.0488
No. pomed (day, 15% C2)	NOx, Ib/MBtu (HHV) as NO2 (Incl. duct burner fuel)	0.1652	0.0324	0.1652	0.0454	0.0438	0.0330	0.0440
No. pomed (day, 15% C2)								
NOx, ppms (etc)								
NOX, permy (vert)								2.0
NOX, Ehris as NOZ (includes NOX mergin applied to CTG)								
NOX, EMBED (LHV) as NOZ (Incl. duct burner Nat)   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.0005   0.000								
NOx, bM8bu (HHV) as NOZ (incl. duct burner Nath)  SCR NH3 silp, permot (day, 15% OZ)  SCR NH3 silp, pe								
SCR NH3 slp, permd (dry, 15% C2)  SCR NH3 slp, permd (dry, 15% C2)  SCR NH3 slp, but  81  82  83  84  84  84  85  85  86  86  86  86  86  86  86  86								
SCR NHO step, bth  8,4 14,9 8,7 25,5 30,9 23,8 30,6 30,6 30,6 30,6 30,6 30,6 30,6 30,6	TOO, SEMINE (1917) 40 ITO2 (INC. USO) DOING 1961/		<u> </u>	V.0315	J.0073	0,0073	0.0073	0.0073
SCR NHO step, bth  8,4 14,9 8,7 25,5 30,9 23,8 30,6 30,6 30,6 30,6 30,6 30,6 30,6 30,6	SCR NH3 site, permed (day, 15% OZ)	50	100	50	100	100	100	100
Strick CO Embalations								30.6
CO, ppmvd (dry), 15% C2)  CO, ppmvd (dry) 15%			1		I	1	10.0	1
CO, ppmvd (dry), 15% C2)  CO, ppmvd (dry) 15%	Stack CO Britishas	THE PARTY OF THE PARTY.	<b>海岭区5.15%的沿地市</b>	Same and the second	<b>明练到发行社。1973年</b>	4445265 SEE	38:22:32:25:0:32:22	MARKET MARKET TO A
CO, permed (eff) CO, pe								10.1
CO, permer (verti) 17.9 8.2 177 14.9 14.0 8.2 14.2 CO, permer (verti) 5.0 19.1 4.0 14.0 8.2 14.2 CO, permer (verti) 5.0 19.1 4.0 14.0 14.5 5.1 14.3 0.0 5.1 1.0 14.0 14.0 14.0 14.0 14.0 14.0 14.		20.0	9.0	20.0				15.8
CO, EMRIS (LHV) (incl. duct burner bue)  CO, EMRIS (LHV) (incl. duct burner bue)  0.0031  0.0032  0.0032  0.0032  0.0032  0.0032  0.0032  0.0032  0.0033  0.0032  0.0032  0.0032  0.0033  0.0032  0.0033  0.0032  0.0031  0.0036  0.0077  0.0036  0.0077  0.0036  0.0077  0.0036  0.0077  0.0036  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.0078  0.00	CO, ppmw (wet)			17.7	14.9	14.0	8.2	14.2
C.O. bM/Blu (HHV) (incl. duct burner fuel)  0.0048  0.0171  0.0059  0.0227  0.0221  0.0188  0.0022  0.0227  0.0221  0.0188  0.022  0.0228  0.0227  0.0221  0.0188  0.0222  0.0228  0.0228  0.0228  0.0238  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.038  0.	CO, Bufn (includes CO margin applied to CTG)							51.0
Stack SOZ Entissions, after SOZ Oxidation   Soz								0.0246
Assumed S2C axidation rate in CO Catalyes, vg/% 0.0% 0.0% 0.0% 0.0% 0.0% 0.0% 0.0% 0.	CO, Ib/MBitu (HHV) (incl. duct burner fuel)	0.0348	0.0171	0.0359	0.0227	0.0221	D.0168	0.0222
Assumed S2C axidation rate in CO Catalyes, vg/% 0.0% 0.0% 0.0% 0.0% 0.0% 0.0% 0.0% 0.								
Assumed SO2 addation rate in SCR, wiffs  3.0% 3.0% 3.0% 3.0% 3.0% 3.0% 3.0% 3.0%								
S02, ppm/d (dry, 15% OZ)								
SO2, ppmed (day)         0.27         0.91         0.28         1.39         1.31         0.94         1.33           SO2, ppmve (wet)         0.24         0.83         0.23         1.22         1.17         0.86         1.18           SO2, bbrh         1.39         4.44         1.28         9.07         9.75         7.10         9.95           SO2, bbrhBlu (LHV) (incl. duct burner fuel)         0.001         0.004         0.001         0.0047         0.0047         0.004         0.004	Assumed SO2 coodstion rate in SCR, vol%	3.0%	3.0%	3.0%	3.0%	3.09	3.09	3.0%
SO2, ppmed (day)         0.27         0.91         0.28         1.39         1.31         0.94         1.33           SO2, ppmve (wet)         0.24         0.83         0.23         1.22         1.17         0.86         1.18           SO2, bbrh         1.39         4.44         1.28         9.07         9.75         7.10         9.95           SO2, bbrhBlu (LHV) (incl. duct burner fuel)         0.001         0.004         0.001         0.0047         0.0047         0.004         0.004							<b>├</b>	
SO2 ppmw (wet)         0.24         0.83         0.23         1.22         1.17         0.86         1.11           SO2, IbM         1.39         4.44         1.28         9.07         9.75         7.10         9.67           SO2, IbM/Bit (J-IV) (Incl. duct burner fuel)         0.0001         0.0044         0.0011         0.0047         0.0047         0.0047         0.0047								
\$02, bith 1.39 4.44 1.28 9.07 9.75 7.10 9.67 \$0.004 \$0.001 0.0047 0.0047 0.0047 0.0047 0.0047								
SO2, Io/MBItu (LHV) (incl. duct burner fuel) 0.0011 0.0044 0.0011 0.0047 0.0047 0.0044 0.001								
	SO2, bM8bu (LHV) (Incl. duct burner fuel) SO2, bM8bu (HHV) (Incl. duct burner fuel)	0.0011	0,0044	0.0011		0.0047		

1/34/2906							
FMPA				i			
Treasure Coast Energy Center Unit 1 Stack & Veatch Project 13889.0030							
1x1 Emissions Estimates Case Number	22	Z3	24	45	50	51	52
				·			
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type CTG Load	Distilate 50%	Netural Gas 50%	Distillate 50%	Natural Gas 100%	Natural Gas 100%	Natural Gas 100%	Natural Gas
CTG triet Air Cooling	orr	Off	Off	011	Evap. Cooler	Evap. Cooler	Off
CTG SteamAVater Injection	Water	No.	Water	No	No.	No.	No
Amblent Temperature, F	26	73	73	100	59	59	59
HRSG Duct Firing	Unfired	Unfired	Unfired	Fired	Fired	Unfired	Fired
Fuel Suffur Content (grams/100 standard cubic feet)	568.31	2.00	568.31	2.00	· 2.00	2.00	2,00
Stack Emissions - continued							
Stack UNC Entailing		3.200 9823586800 perfe		200 <b>2 - W</b>		1887 P. 1897 S. 1898	900000000000000000000000000000000000000
UHC, ppmvd (dry, 15% C2)	5.6	6.7	5.9	17.4	16.0	6.4	18.2
UHC, pprmd	7.8	7.7	7.9	28.7	24.9	7.6	25.3
UHC, ppmw UHC, th/h as CH4 (includes correction adder)	7.0	7.0	7.0 10.0	25.1 46.9	22.3 46.5	7.0	22.7 46.7
UHC, Ib/MBtu (LHV) (Incl. duct burner fuel) UHC, Ib/MBtu (HHV) (Incl. duct burner fuel)	0.0082	0.0093 0.0084	0.0089 0.0084	0.0243 0.0219	0.0222	0.0090	0.0225
Stack YOC Emissions	TO BEEN LODGERED OF	\$1000700000 (ASSESSED ASSESSED	SINECTON TO	4000 C (8000 C)	#### 1.47T   SECTION 2	Control Marian	200
VOC, ppmvd (dry, 15% O2)	2.8	1.3	2.9	1.8	1.7	1.3	1.7
VOC, pprivd (dry)	3.9	1.5	4.0	3.0	2.7	1.5	2.7
VOC, ppmw (wet)  VOC, fb/h as CH4 (includes VOC correction as applied to CTG)	3.5	1.4	3.5 5.0	2.6 4.9	2.4 5.0	1.4	2.4 5.0
VOC, but as CH4 (includes VOC correction as appared to CH5)  VOC, butMBtu (LHV) (incl. duct burner fuel)	0.0041	0,0019	0.0045	0.0025	0.0024	0.0018	0.0024
VOC, Ib/MBtu (HHV) (Incl. duct burner fuel)	0.0039	0.0017	0.0042	0.0023	0.0022	0.0018	0.0022
COMMANDE OF THE PROPERTY OF TH	Car Bankson washington and income.						v mor can are a community
PM10 without the Effects of SO2 oxidation	is the comment of the	provinces of the	100.500 to 100.000 to 1	(A. 245) (S. 185) (S. 186)		77 W. F. (877)	
PM10 Emissions - Front Half Catch Only PM10, Io/h	17.0	9.0	17.0	14.7	14.3	9.0	14.4
PM10, Io/MStu (LHV) (Incl. duct burner fuel)	0.0140	0.0069	0.0151	0.0076	0.0069	0.0056	0,0069
PM10, fb/MBtu (HHV) (Incl. duct burner fuel)	0.0132	0.0060	0.0142	0.0068	0.0062	0.0050	0.0063
PM10 Emissions - Front and Back Half Catch						l	
PM10, b/n	34.0 0.0290	18.0	34.0	31.6 0.0163	30.8	18.0 0.0112	31.0
PM10, Ib/MBh: (LHV) (Incl. duct burner fuel) PM10, Ib/MBh: (HHV) (Incl. duct burner fuel)	0.0263	0.0178 0.0161	0.0284	0.0147	0.0147	0.0112	0.0149
PM10 with the Effects of SQ2 Oxidation [Includes (IMM32-(SQ4)]		0.0161	0.0254	0.0(4)	0.0133	0.0101	0,0133
PM10 Emissions - Front Half Catch Only							Anger-Management and Calcular Security
PM10, Ib/h	17.0	9.0	17.0	14,7	14.3	9.0	14.4
PM10, Ib/M8tu (LHV) (incl. duct burner fuel)	0.0140	0.0069	0.0151	0.0076	0.0069	0.0056	0,0069
PM10, Ib/M8tu (HHV) (incl. duct burner fuel)	0.0132	0.0080	0.0142	0.0068	0.0062	0.0050	0,0063
		<b>!</b> — — —					
PM10 Emissions - Front and Back Helf Catch PM10 b/h	35.2	22.0	35.1	38.0	37.9		38.0
PM10, to/MBtu (LHV) (Incl. duct burner fuel)	0.0290	0.0218	0.0313	0.0197	0.0181	24.3 0.0151	0,0183
PM10, 8xMStu (HHV) (incl. duct burner fuel)	0.0273		0.0294	0.0177	0.0163	0.0136	0.0165
Total Effects of SO2 Oxidation	95 (0:57 160000 co-50)	54 (0.54)	200		B. 10.44.20 34.71	578/3800 et 2 10/1900	200000000000000000000000000000000000000
Total SO2 to SO3 conversion rate, %vol	30,29	30.2%	30.2%	25.6%	26.1%	30.2%	28.1%
Total Amount of SO2 converted to SO3, Ib/h	0.50		0.55	3.11	3.45	3.05	3.41
Maximum Stack Ammonium Sulfate [(NH4)2-(SO4)] (assuming 100% conversion from SO3), b/h	1.24		1.14		7.12	6.32	7.03
Maximum Stack H2SO4 (assuming 100% conversion from SO3 to H2SO4), lb/h	0.92	2.94	0.85	4.77	5.28	4.69	5.22
Post Combustion Emissions Control Equipment		<del>-1</del>		<u> </u>			
* *			E 1	Tallian III			
Selective Catalytic Rictiction (SCR)		10,481	AA.3938	2004-2004-200			100000000000000000000000000000000000000
NOx removed in SCR, 16wt	81,09 172,9	77.8%	81.09 159.9	84.0%	83.4%	77.8% 45.9	83.5% 84.5
Ammonia Sip, Ib/h	9.4		159.9		30.9		
			<u></u>	15.0			
Notes:  1. The enrissions estimates shown in the table above are per stack.  2. The dry sir composition used is 0.95% Ar, 78.05% N2 and 20.95%.02  3. Standard conditions are defined as 80 F, 14.650 pala, Norm conditions are defined as 0 C, 1.103 bar  4. All open values are based on CH4 catheristic pass.  5. The CTG performance is from GTP, a General Electric estimation program.  6. The HOD increase in the SSC restayle in negligible and not included in the serveysis.  7. The VOCUHC rate is assumed to be 20% for NG and 50% for distillate.  8. Anymorthum sublates created downstream of the SSCR are included in the back half particulates. The essumption that 100° SOI is converted to anymorthum sublates results in 'worst case' particulate emissions.  9. Where manufacturer date of Eth of pollutant emissions were available, the greater of the manufacturer's estimate and 88' estimate was used in the summary table, is the 884' estimate were adulated, the greater specification.							
<ol> <li>Duct burner emissions are included. The duct burner pollutant emissions are Black &amp; Vestch estimates based on low NO duct burner emissions data (provided by Forney).</li> </ol>	Ox.						

TCEC Unit 1 Emissions Data.xls

The front half catch of CT perticulate emissions is essumed to be half the amount of the front and back half catch.
 As requested the SCR was designed to reduce the NOx stack emissions to 2 and 8 perivedig 15%O2 when firing NG and Distillate, resourchedy.
 The emissions estimate is based on FGT gas with a maximum subtar content of 2.0 grains/100acf.

1/14/2905 FMPA							
Tressure Coast Energy Center Unit 1							
Black & Vestch Project 138359.0030 1x1 Emissions Estimates							
Case Number	53	54	55	56	57	58	59
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type CTG Load	Natural Gas 100%	Natural Gas 75%	Natural Gas 50%	Natural Gas 100%	Distillate 100%	Distillate 100%	Distillate 100%
CTG Inlet Air Cooling	Off	Off	Off	Evap. Cooler	Off	Evap. Cooler	Off
CTG Steam/Water Injection Ambient Temperature, F	No Se	No. 59	No. 59	No 100	Water 59	Water 59	Water 59
HRSG Duct Firing	Unfired	Unfired	Unfired	Fired	Fired	Fired	Unfired
Fuel Suthur Content (grains/100 standard cubic feet)	2.00	2.00	2.00	2.00	568.31	568.31	566.31
Ambient Conditions							
Ambient Temperature, F	59.0		59.0	100.0	59.0	59.0	59.0
Ambient Relative Humidity, % Atmospheric Pressure, pais	60.0 14.690	50.0 14.690	60.0 14.690	48.4 14.690	60.0 14.690	60.0 14.690	50.0 14.690
Autophreic Pressure, pare	1 (4,050)	14.090 ]	14.080	14.090	14,090	14.090 )	14.030 )
Combustion Turbine Performance							
CTG Performance Reference	GTP	GTP	GTP	GTP	GTP	GTP	GTP
CTG Inlet Air Conditioning Effectiveness, %	0			85	0	85	
CTG Compressor triet Dry Buth Temperature, F	59.0 60.2	59.0	59.0	85.2 89.7	59.0	52.6 92.9	59.0 60.2
CTG Compr. thlet Relative Humidity, %		60.2	60.2	89.7	50.2		
Infet Loss, in. H2O Exhaust Loss, in. H2O	4.0 15.0	4.0	4,0 6,9	4.0 13.2	4.0 13.2	4.0 13.2	4.0 13.2
CTG Load Level (percent of Base Load) Gross CTG Output, KW	100% 169,000	75% 126,800	50% 84,500	100% 154,500	100%	100%	179,600
	9,390	10,230	12,270	9,650	10,150	10,120	10,150
Gross CTG Heat Rate, Stu/kWh (LHV) Gross CTG Heat Rate, Stu/kWh (HHV)	10,416	10,230	13,611	10,705	10,810	10,778	10,810
CTG Heart Input, MBturh (LHV)	1,586.9	1,297.2	1,036,8	1,490.9	1,822.9	1,841.8	1,822.9
CTG Heat Input, MSturh (HHV)	1,760.3	1,438.9	1,150.1	1,653.9	1,941.4	1,961.6	1,941.4
CTG Water/Steam Injection Flow, (b/h				0	135,980	135,030	135,980
Injection Fluid/Fuel Ratio	0.0	0.0	0.0	0.0	1.4	1.3	1.4
CTG Exhaust Flow, Ib/h	3,602,000	2,904,000	2,403,000	3,357,000	3,763,000	3,806,000	3,763,000
CTG Exhaust Temperature, F	1,116	1,161	1,200	1,148	1,098	1,092	1,098
Compustion Turbine Fuel	CESSON SECTION	5/6/8 T 14/6 15/6		\$100 (E. 200 VOG)		37 75.66	
Total CTG Fuel Flow, forh CTG Fuel Temperature, F	76,240 385	62,320 365	49,810 365	71,520 365	99,610	100,650 60	99,610 60
CTG Fuel LHV, Blurib	20,815	20,816	20,816	20,816	18,300	18,300	18,300
CTG Fuel HHV, Btuffb	23,091	23,091	23,091	23,091	19,490	19,490	19,490
HHV/LHV Ratio	1,1093	1.1093	1.1093	1.1093	1.0650	1.0650	1,0850
CTG Fuel Composition (Ultimate Analysis by Weight)							
C C	0.00% 73.76%	0.00% 73.76%	0.00% 73.76%	0.00% 73.76%	0.00% 85.00%	0 00% 85.00%	0.00% 85.00%
M2	24.01% 0.61%		24.01% 0.81%	24.01% 0.61%	14.80%	14.80%	14.80%
02	1,61%	1.61%	1.61%	1.61%	0.00%	0.00%	0.00%
	0.00657%	0.00857%	0.006\$7% 100.00%	0.00657% 100.00%	0.00150%	0.00150%	0.00150%
Fuel Suffur Content (grains/100 standard cubic feet)	2.00	2.00	2.00	2.00	568.31	566.31	566.31
Combustion Turbine Exhaust					• • •		
CTO Exhaust Analysis (Volume Basis - Welt)	1 - 12965-012-20403	100 July 100 100 100 100 100 100 100 100 100 10	200 (200 )	50895555.2A			
	0,93%	0.93%	0.94%	0.91%	0.89%	0.89%	0 89%
C02 H2O	3.69% 8.15%	3.74% 8.25%	3.62% 8.00%	3.69% 10.71%	5.28% 12.07%	5.28% 12.17%	5.28% 12.07%
N2	74,45%	74,41%	74.50%	72.44%	70.75%	70.67%	70.75%
O2 SO2, (after SO2 oxidation)	12,78% 0.00010%	12.67%	12.94% 0.00010%	12.25%	0.00003%	11.00% 0.00003%	0,00003%
SO3, (after SO2 oxidation)	0.00002%	0.00002%		0,00002%	0.00001%	0.00001%	0.00001%
Total							
Molecutar Wt, Ib/mol Specific Volume, R*3/Ib	28 41 39.06	28.41 40.68	28,42 41,94	28.13 40.43	28.20 39.08		28.20 39.08
Specific Volume, act/fb	13.36	13.36	13,36	13.49	13.45	13.46	13.45
Exhaust Gas Flow, acfm Exhaust Gas Flow, acfm	2,344,902 801,445	1,968,912 646,624	1,679,697 534,668	2,262,059 754,768	2,450,967 843,539	2,470,094 853,813	2,450,967 843,539
CTG NOx Entestions (Without Post Combustion Emissions Control)	*	1041. 480 084000		2000 2000 2010 201	1986		
Additional Percent Margin included in mass based NOx Emissions below	0%	0%	0%	0%	0%		0%
NOx, ppmvd (dry, 15% O2)	9.00	9.00	9.00	9.00	42.00	42.00	42.00
NOx, ppmvd (dry)	10.60	10.80	10,40	10.90	59.40	59.40	59.40
NOx, ppmw (wet) NOx, Bith as NO2	9.80 58.0	47.0	37.2	55.0	52.20 322.1	325.5	52.20 322.1
NOx, IdMBtu (LHV) NOx, IdMBtu (HHV)	0.0365	0.0362	0.0359 0.0324	0.0369	0.1767 0.1659	0.1767	0.1767 0.1659
			I	i		1	
CTG CO Entisators (Without Post Combination Entisators Control)  Additional Percent Margin included in mass based CO Emissions below	0%	0%		0%	09		09
CO, pprind (dry, 15% OZ) CO, pprind (dry)	7.60 9.00	7.50 9.00					14.10
CO, ppmw/ (wet) CO, bb/h	8.30 29.4	8.30 24.0	8.30	8.00		17.60	17.60 65.9
CO, Ib/MBtu (LHV)	0 0185	0.0185	0.0193	0 0181	0.0361	0 0361	0.0361
CO, to/MBtu (HHV)	0.0167	0.0167	0.0174	0.0163	0.0339	0.0339	0 0339
CTG 602 Emissions (After 602 Oxydation, Without Post Combustion Emissions Control)		SOUTHER STREET	\$3000 - J. \$600 C	52802264 (J88	Section of the sectio		29/24/05/90/1865
Additional Percent Margan included in bt/h SO2 Emissions below Assumed SO2 oxidation rate in CTG, vol16	20.0%	20.0%	20,09	0.0%		0.0%	20.01
SO2, pprivid (dry, 15% O2)	0.9083	0.9083	0.9083	0.9083	0.2247	0.2247	
SO2, pprived (dry)	1.0734	1.0892	1.0499	1.1019	0.3177	0.3177	0.2247 0.3177
SO2, ppmw (wet)	0.9859 8.0068	0.9994 6.5449	0.9658 5.2311	0.9839 7.5216	0.2794 2.3884		0.2794 2.3884
SO2, Ib/MBtu (LHV)	0.0050	0.0050	0.0050	0.0050	0.0013	0.0013	0.0013
SO2, IDMBtu (HHV)	0.0045	0.0045	0.0045	0 0045	0.0012	0.0012	0.0012

1/14/2008					1		
FMPA				Į.			
Treasure Coast Energy Center Unit 1				Į.	i		
Black & Vestch Project 138859.0030 1g1 Emissions Estimates							
Case Number	53	54	55	56	57	58	59
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type	Natural Gas	Natural Gas	Natural Gas	Natural Gas 100%	Distillate 100%	Distillate 100%	Distillate 100%
CTG Load CTG Inlet Air Cooling	100%	75% Off	50% Off	Evap. Cooler	Off	Evap. Cooler	Off
CTG Steam/Water Injection	No.	No.	No	No.	Water	Water	Water
Ambient Temperature, F	59	59	59	100	59	59	59
HRSG Duct Firing	Unfired	Unfired	Unfired	Fired	Fired	Fired	Unfired
Fuel Sulfur Content (grains/100 standard cubic feet)	200	2.00	2.00	2.00	566.31	566.31	566.31
Combustion Turbine Exhaust - continued							
CTO LINC Emissions (Without Post Combustion Emissions Control)	9838888668650000	2 . 201-12622 21 2022 2	24-27-1 (ERFERENCE)	Y SERVED VESTORIOR	786000000000000000000000000000000000000	26/2021/2021/2021/2021	SHANWEN MEDICE
Additional Percent Margin included in 80/h UHC Emissions Below	0.0%	0.0%	0.0%	0.0%	0.0%	0.0%	0.0%
UHC, pprivd (dry, 15% O2)	5.4	6.4	6.6	6.5	5.6	5.6	5.6
UHC, ppmwd (dry)	7.6	7.6 7.0	7.6 7.0	7.8 7.0	8.0 7.0	8.0 7.0	8.0 7.0
UHC, ppmvv (wet) UHC, tb/h as CH4	14.2	11.5	9.5	13.4	15.0	15.2	15.0
UHC, Ib/MBtu es CH4 (LHV)	0.0090	0.0089	0.0092	0,0090	0.0082	0.0082	0.0082
UHC, Its/MBtu as CH4 (HHV)	0.0081	0,0080	0.0083	0.0081	0.0077	0.0077	0.0077
CTG VOC Emissions (Without Post Combustion Emissions Control)		1200 C 100 C	887 Y S S S S S S S S S S S S S S S S S S	0.14		100 PM	10.704-10.006-20.00
Additional percent margin included in Ibth VOC emissions below	0%	0%	0%	0%	0%	0%	- 0%
VOC percentage of UHC	20%	20%	20%	20%	50%	50%	50%
VOC, ppmvd (dry, 15% O2)	1.3	1.3	1.3	1.3		2.8	2.8
VOC, pprivd (dry)	1.5		1.5	1.6		4,0	4.0
VOC_ppmww (wet)	1.4		1.4	1.4	3.5	3.5	3.5
VOC, Ibrh as CH4	2.8	2.3	1.9	2.7	7.5	7.6	7.5
VOC, Ib/MBtu as CH4 (LHV)	0.0018	0.0018	0.0018	0,0018	0.0041	6 0041	0.0041
VOC, Ib/MBtu as CH4 (HHV)	0.0016	0.0016	0.0017	0.0016	0.0039	0.0039	0,0039
CTG PM10 Emissions (without the Effects of SOZ Cixidation)		-5825-00-286-A-28988	DO TRANSPORTE SERVICE	(0.00) (0.00) (0.00) (0.00) (0.00)		V. 10. (2. 1) A. (2. 1)	
Percent margin included in PM10 emissions below	0%	0%	0%	0%	0%	0%	0%
PERCENTION OF THE PARTY OF THE				, , , , , , , , , , , , , , , , , , ,			
PM10 Emissions - Front Half Catch Only							
PM10, b/h	9.0	9.0	9.0	9.0	17.0	17.0	17.0
PM10, Ib/MBtu (LHV)	0.0057	0.0069	0.0087	0.0060	0.0093	0.0092	0.0093
PM10, IbMBtu (HHV)	0.0051	0.0063	0,0078	0.0054	0.0088	0.0087	0.0088
PM10 Emissions - Front and Back Half Catch	1				<del></del>		
PM10, Ib/h	18.0	18.0	18.0	18.0	34.0	34.0	34.0
PM10, IbM8tu (LHV)	0.0113		0.0174	0.0121	0.0187	0.0185	0.0187
PM10, IbMBtu (HHV)	0.0102	0.0125	0.0157	0.0109	0.0175	0.0173	0,0175
KRSG Duct Burners							
					1		
Diet Burner Piet	NAMES OF STREET	NECTO PROPER	100000000000000000000000000000000000000	90/b36/06/60/06/60/06/60/	12-12-12-12-12-12-12-12-12-12-12-12-12-1	A MARKAGO PART A STATE OF	
Duct Burner Heat Input, MBtu/h (LHV)	0.0	0.0	0.0	499.6		499.6	0.0
Duct Burner Hest Input, MBtu/n (HHV)	0.0			554.2		554.2	0.0
Total Duct Burner Fuel Flow, Is/h	0	•	0	24,000	23,950	24,000	
	1	<del> </del>			<del>                                     </del>	<u> </u>	<b>├</b>
Duct Burner Fuel LHV, Btu/lb	20,816	20,816	20,816	20,816	20,816	20,815	20,816
Duct Burner Fuel HHV, Blufts	23,091	23,091	23,091	23,091	23,091	23,091	23,091
				<del></del>			
Duct Burner Fuel Composition (Ultimate Analysis by Weight)		<del> </del>					ļ <u></u> -
	0.00%	0.00%	0.00%	0.00%		0.00%	0.00%
<u>с</u> н2	73.76% 24.01%	73.76%	73.76%	73.76% 24.01%		73.76% 24.01%	73.76% 24.01%
N2	0.61%						
02	1.61%						
	0.00657%			0.00657%	0.00657%		
Total	100 0%	100.0%	100,0%	100.0%	100.0%	100.0%	100.0%
Fuel Suffur Content (grains/100 standard cubic feet)	2.00	2.00	2.00	2,00	2.00	2.00	2.00
	and and address of the Control of the	Sept of word Control of the American Co.	00000000000000000000000000000000000000	NO. NO. SECTIONS OF MANY ACCOUNTS	The real and the second second second	200000000000000000000000000000000000000	
Duct Burner Entestors	. AND THE REAL PROPERTY CONTROL OF THE PARTY CONTRO			0.000		92 90 90 90	
Duct Burner NOx, fo/MBtu (HHV)  Duct Burner CO, fo/MBtu (HHV)	0.080	0.080	0.080	9.080 0.040		0.080	0.080
Duct Burner CO, IbMBRu (HHV)  Duct Burner UHC (as CH4), IbMBRu (HHV)	0.040			0.040		0.040	
Duct Burner VOC (as CH4), Ib/MBtu (HHV)	0.004						
Duct Burner PM10, Its/MBtu (HHV) (front helf catch only)	0.010	0.010	0.010				
Duct Burner PM10, Ib/MStu (HHV) (front and back half catch)	0.024	0.024					
			<del> </del>	<del></del>		ļ	<b> </b>
Assumed SO2 oxidation rate in Duct Burner, vot% Total SO2, Ibth from Duct Burner Fuel only (after SO2 oxidation)	10.0%						
Total SO2, but from Duct Burner Fuel only (after SO2 cookpon)  Total SO3, but from Duct Burner Fuel only (after SO2 cookpon)	0.000						
t Annu manufactures transfer the time to make the factor of the manufactures.	1	5.500	1	0.354	- v.sss	0.354	1 0.00
DB NCx, byh	0.00	0.00	0.00	44.30	44.20	44.30	0.00
DB CO, birth	0.00	0.00	0.00	22.20	22.10	22.20	0.00
DB UHC (as CH4), ib/h	0.00						0.00
DB VOC (as CH4), fb/h	0.00						
DB PM10, lib/t (front half catch only) DB PM10, lib/t (front and back half catch)	0.00						

1/14/2006							
FMPA							
Treesure Coast Energy Center Unit 1							
Black & Vesich Project 138869.0030							
1x1 Errissions Estimates							
Case Number	53	54	55	56	57	56	59
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type	Naturai Ges	Natural Gas	Natural Ges	Natural Ges	Distillate	Distillate	Distillate
CTG Load	100%	75%	50%	100%	100%	100%	100%
CTG Intel Air Cooling	Ott	Off	Off	Evap. Cooler	Ott	Evrep. Cooler	Off
CTG Steam/Water Injection	No	No	No	No	Water	Water	Water
Ambient Temperature, F	59	59	59	100	59	59	56
HRSG Duct Firing	Unfired	Unfired	Unfired	Fired	Fired	Fired	Unfired
Fuel Sulfur Content (grains/100 standard cubic feet)	2.00	2.00	2.00	2.00	566.31	565.31	566.31
Stack Emissions							
Stack Exhaust Analysis - Votune Basis - Wet 1988 - Through the Analysis - Votune Basis - Wet 1988 - Through the Analysis - Votune Basis - Wet 1988 - Through the Analysis - Votune Basis - Wet 1988 - Through the Analysis - Votune Basis - Wet 1988 - Through the Analysis - Votune Basis - Wet 1988 - Through the Analysis - Through the Analysis - Votune Basis - Wet 1988 - Through the Analysis -	いていることの大学を影響	<b>光大型网络路径工机场</b>	ST CASK TO RELIGIOUS	元后-765000000000000000000000000000000000000	2012年では1960年を記せ	2000年7年2月1日	4566 MIX \$475968F
At	0.93%	0.93%	0.94%	0 90%	0.88%	0.88%	0.89%
CO2	3.69%	3.74%	3.62%	4.86%	6.32%	6.30%	5.28%
H2O	8.15%	8.25%	8.00%	12.95%	14.06%	14.14%	12.07%
N2	74,45%	74.41%	74.50%	71.58%	70.00%	69.92%	70.75%
02	12.78%	12.67%	12.94%	9.71%	8.75%	8.76%	11.01%
SO2 (after SO2 oxidation)	0.000090%	0.000090%	0.000080%	0.000120%	0.000040%	0.000040%	0.000020%
SO3 (after SO2 coddation)	0.000040%	0.000040%	0.000040%	0.000040%	0.000030%	0.000030%	0.000020%
Total	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%	100.0%
Stack Exit Temperature, F	180	169		169	251	251	262
Stack Diameter, ft (estimated)	18	18	18	18	18	16	18
Stack Flow, Ib/h	3,601,997	2,903,997	2,402,998	3,380,996	3,786,948	3,829,998	3,762,999
Stack Flow, softm	801,445	646,624	534,668	763,543	852,695	863,027	843,539
Stack Flow, actm	986,348	782,144	638,397	924,140	1,167,012	1,180,917	1,172,175
Stack Edt Velocity, ft/s	65.0	51.0	42.0	61.0	76.0	77.0	77.0
·							
Stack NOx Emissions without the Effects of Selective Cutalytic Reduction (SCR)	がいめなりらんが発生的な	ANT TERROL OF ELABORS	1.57节期的自然发现	The state of the s	平方位 医视频器 网络木木	100 March 2000	STATE OF THE STATE
NOx, ppmvd (dry, 15% O2)	9.0	9.0	9.0	12.3	37.9	37.9	42.0
NOx, ppmvd (dry)	10.6	10.8	10.4	20.2	68.4	68.3	59.4
NOx, ppmw (wet)	9.8	9.9	9.6	17.6	58.8	58.7	52.2
NOx, bith as NO2 (includes correction adder)	58.0	47.0	37.2	99.3	366.4	369.8	322.1
NOx, Ib/MBtu (LHV) as NO2 (incl. duct burner fuel)	0.0365	0.0362	0.0369	0.0499	0.1578	0.1579	0.1767
NOx, Ib/MBbu (HHV) as NO2 (incl. duct burner fuel)	0.0329	0.0327	0.0324	0.0450	0.1469	0.1470	0.1659
Stack NOx Endssions with the Effects of Selective Cutalytic Reduction (SCR)		GRADIEN STREET	ANNALY CONTRACT	0760A00000	THE HEART STARTS	Selection of the last of the l	anticate source enterent
NOx, ppmed (dry, 15% O2)	2.0	20		2.0	6.0	8.0	8.0
NOx, pprivd (dry)	2.4	24		3.3	14.4		11.3
NOx, pornw (wet)	22	2.2	2.1	2.9	12.4		9.9
NOx, b/h as NO2 (includes NOx margin applied to CTG)	12.9	10.4	8.3	16.1	77.3	78.0	51.4
NOx, bMBtu (LHV) as NO2 (incl. duct burner fuel)	0.0081	0.0081	0.0080	0.0061	0.0333	0.0333	0.0337
NOx, Ib/MBtu (HHV) as NO2 (incl. duct burner fuel)	0.0073	0.0073	0.0072	0.0073	0.0310	0.0310	0.0316
000 WIR						<del></del>	
SCR NH3 stip, pprivid (dry, 15% O2)	10.0	10.0	10.0	10.0	5.0		5.0
SCR NH3 nlip, fb/h	23.4	19.2	15.3	29.4	17.8	18.0	14.1
THE THE PROPERTY WAS A STATE OF THE PROPERTY O	C.C. Tree E. Terre In Grand St.	TOPHOLOGICAL VIOLEN	0.07 8/14 (0.0888)	112.7		200000000000000000000000000000000000000	TO US TO SERVICE OF
Stack CO Emissions							
CO, pprint (dry, 15% O2)	7.6			10.1	15.0		14.1
CO, ppmed (dry)	9.0	9.0		16.6		27.0	20.0
CO, ppmw (wet)	29.4	240		14.5			17.6 65.9
CO, toth (includes CO mergin applied to CTG)	0.0185	00185		0.0247			0.0361
CO, toMBtu (LHV) (incl. duct burner fuel)	0.0185	0.0185	0.0193	0.0247	0.0379		0.0381
CO, to/MBtu (HHV) (incl. duct burner fuel)	3.0167	3.0167	0.0174	0.0223	0.0363	0.0363	0.0339
Stack SO2 Emissions, after SO2 Oxidation	No. 0000000 4 80	77.47748334444090249008	(CO205) (C. SON) (C. SON)		-0755 Ratio 2757 Basis 286	578.1/1.1408.407877M25.449	2004 (1940) Set (1940)
Assumed SO2 addation rate in CO Catalyst, vol%	0.0%	0.0%		0.09	20.09	in Manual 2n - 1 , doubt and additional series	20.09
Assumed SO2 coddation rate in CO Catalyst, vol% Assumed SO2 coddation rate in SCR, vol%	3.0%	3.0%		3.09			
ASSUMED SO 2 DECEMBER 18 SUT, 1979	3,0%	3.0%	3.0%	3.04	3.09	3.09	3.09
SO2, ppmvd (dry, 15% O2)	0.79	0.79	0.79	0.84	0.29	0.29	D.16
	0.79	0.79	0.79	1.38	0.29		0.22
SO2, ppmyd (dry)	0.94	0.95	0.92	1.38			
SO2, ppmw (wet)	6.99	5.71		9.32			0.20
	0.0044	0.0044		9.32 0.0047			1.67
SO2, bMBtu (LHV) (incl. duct burner fuel) SO2, bMBtu (HHV) (incl. duct burner fuel)							
	0.0040	0.0040	0.0040	0.0042	0.0015	0.0015	0.0006

1/14/2006 FMPA							
FMPA Treesure Coest Energy Center Unit 1							
Black & Veatch Project 132269.0030							
1x1 Emissions Estimates							
Case Number	53	54	55	56	57	58	59
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type	Natural Gas	Natural Gas	Natural Gas	Natural Gas	Distillate	Distillate	Distillate
CTG Load	100%	75%	50%	100%	100%	100%	100%
CTG triet Air Cooling CTG Spram/Water Injection	Off No	Off	Off No	Evap. Cooler	Off Water	Evap. Cooler Water	Off Water
Ambient Temperature, F	59	59	, ND 59	100	59		vvater 59
HRSG Duct Firing	Unfired	Unfired	Unfired	Fired	Fired	Fired	Unfired
Fuel Sulfur Content (grains/100 standard cubic feet)	2.00	2.00	2.00	2.00	566.31	568.31	568.31
Stack Emissions - continued							
Stack UHC Emissions	LO MARABOTANIA	2000 1 100 A	244364200 200	alionners (1886)	A CONSERVATION OF P.	81.00.45 (0.00) 412 GP	HAP \$60000000
UHC, pprivd (dry, 15% O2)	6.4	6.4	6,6	16.8	14.4	14.3	5.6
UHC, pprove	7.6	7.6	7,8 7.0	27.7	25.9 22.3	25 8 22.1	B.0 7.0
UHC, Ib/h as CH4 (Includes correction adder)	14.2	11.5	9.5	46,7	48.2	48.4	15.0
UHC, IbMBtu (LHV) (incl. duct burner fuel)	0.0090	0.0089	0.0092	0.0234	0.0207	0.0207	0.0082
UHC, fb/M8tu (HHV) (incl. duct burner fuel)	0.0081	0.0080	0.0083	0.0211	0.0193	0.0192	0.0077
Stack VOC Emissions	SOW COMMERCIAL CONTROL	Decements strong	(10-10) (Share 10)	200 X 24 40 00 00 00 00 00 00 00 00 00 00 00 00	2755860004 (SAMESA	- 84-	20.7.0000000000000000000000000000000000
VOC, ppmvd (dry, 15% O2)	1.3	1.3	1.3	1,8	2.9	2.9	2.8
VOC, ppmyd (dry)	1.5	1.5	1,5	2.9	5.2	5.2	4.0
VOC, pprnvw (wet)	1.4		1,4	2.5	4.5	4.5	3.5
VOC, bith as CH4 (includes VOC correction as applied to CTG)  VOC, Ib/MStu (LHV) (incl. duct burner fuel)	2.8 0.0018	2.3 0.0018	1,9 0.0018	4.9 0.0025	9.7 0.0042	9.8 0.0042	7.5 0.0041
VOC, Ib/MBtu (HHV) (incl. duct burner fuel)	0.0016	0.0016	0.0017	0.0022	0.0039	0.0039	0.0039
PM10 without the Effects of 802 oxidation	ASP BRIDE BRIDGES	200 Ballin (1966)	SECTION SECTION	projectore and contract the contract traces.	778 V. (S. (S. (S. (S. (S. (S. (S. (S. (S. (S	photo:	CAMP CONTRACTOR
PM10 Emissions - Front Half Catch Only PM10, b/h	90	90	9.0	14.5	22.5	22.5	17.0
PM10, Is/MBtu (LHV) (incl. duct burner fuel)	0.0057	0.0069	0.0087	0.0073	0.0097	0.0096	0.0093
PM10, Ib/MBtu (HHV) (Incl. duct burner fuel)	0,0051	0.0063	0.0078	0.0066	0,0090	0,0090	0.0088
PM10 Emissions - Front and Back Half Catch PM10, b/h	18.0	18.0	18,0	31.3	47.3	47.3	34.0
PM10, Ib/MStu (LHV) (incl. duct burner fuel)	0.0113	0.0139	0.0174	0.0157	0.0204	0.0202	0.0187
PM10, ib/MBtu (HHV) (incl. duct burner fuel)	0.0102		0.0157	0.0142	0.0190	0.0188	0.0175
PM10 with the Effects of SO2 Oxidation [Includes [10412-[804]]	cari epitelijani	\$	\$ 00 14 A 4 B 100 12	921-20 SM 5-16	SATE STATE	**************************************	Carrier Control Control
PM10 Emissions - Front Half Catch Only PM10, brh	90	9.0	9.0	14,5	22.5	22.5	17.0
PM10, Ib/MBtu (LHV) (Incl. duct burner fuel)	0.0057	0.0089	0.0067	0.0073	0.0097	0.0096	0.0093
PMt0, Ib/MBtu (HHV) (Incl. duct burner fuel)	0.0051	0.0063	0.0078	0.0066	0.0090	0.0090	0.0088
PM to Emissions - Front and Back Half Catch		<b>!</b> — — —				<b>-</b>	<b></b>
PM10. b/h	24.2	23.1	22.1	38.0	51.9	52.0	36.7
PM10, Ib/MBtu (LHV) (Incl. duct burner fuel)	0.0153	0.0178	0.0213	0.0191	0.0224	0.0222	0,0201
PM10, b/MStu (HHV) (Incl. duct burner fuel)  Total Fithers of SCO Outstation	0.0138	0,0160	0.0192	0.0172	0.0208	0.0207	0.0189
Total Effects of SQ2 Chitastion Total SQ2 to SQ3 conversion rate, %vol	30.29	30.2%	30.2%	25.8%	37.0%	37.0%	44,19
Total Amount of SO2 convented to SO3, bift	3.02	2.47	1.97	3.24	2.27	2.28	1,32
Maximum Stack Ammonium Sulfate ((NH4)2-(SO4)) (assuming 100% conversion from SO3), b/h	6.23	5.09	4.07	6.67	4.67	4.71	2.72
Maximum Stack H2SO4 (assuming 100% conversion from SO3 to H2SO4), fb/h	4.62	3.78	3.02	4.95	3.47	3.49	2.02
							<u></u>
Post Combustion Emissions Control Equipment				•			
Selective Catalytic Raduction (SCR)	NAME OF THE PARTY	\$3500.0000000000000000000000000000000000	20000000	CONTRACTOR (	(3.02) (A. 19)		28 9
NOx Removed in SCR, Newt NOx removed in SCR, Buth	77.8% 45.1	77.8%	77.8% 29.0	83.8%	78.9% 289.1	78.99 291.8	81.0% 260.8
Ammonia Sip, Ibrh	23.4	19.2	15.3	29.4	17.8	18.0	14.1
						<u> </u>	
Notes:							
1. The emissions estimates shown in the table above are per stack. 2. The dry air composition used is 0.98% Ar, 78.03% N2 and 20.99%O2.							
The dry air composition used is 0.50% Ar, 76.03% Az and 20.50%-02     Standard conditions are defined as 60 F, 14.696 pata, Norm conditions are defined as 0 C, 1,103 bar							
4. All ppm values are based on CH4 calibration gas.							
S. The CTG performance is from GTP, a General Electric estimation program.							
6. The H2O increase in the SCR catalyst is negligible and not included in the analysis,							
7. The VOC/UHC ratio is assumed to be 20% for NG and 50% for distillate.	Armer .						
<ol> <li>Ammonium suffaces created doenstream of the SCR are included in the back half particulates. The assumption that t SO3 is converted to ammonium suffaces results in "world case" particulate emissions.</li> </ol>	u.rs						
<ol><li>Where manufacturer data of 85h of pollutant emissions were available, the greater of the manufacturer's estimate and</li></ol>	B&Va						
estimate was used in the summary table, i.e. the S&V estimates were adjusted, where applicable.							
10. Duct burner emissions are included. The duct burner pollutant emissions are Black & Vestch estimates based on to	NOx						
that human emissions data (provided by Forney).							

The front half catch of CT perticutate emissions is assumed to be half the emount of the front and back half catch.
 As requested the SCR was designed to reduce the NOs stack emissions to 2 and 8 pprinting 15%O2 when firing NG and Distribute, respectively.
 The emissions estimate is based on FGT pas with a maximum suffur content of 2.0 preins/100sct.

1/14/2005						
FMPA Tressure Coast Energy Center Unit 1						
Black & Vestch Project 138559.0030 1x1 Emissions Estimates						
TXT Emission's Estimates  Case Number	60	61	62	63	64	65
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type CTG Load	Distillate 100%	Distillate 75%	Distillate 50%	Natural Gas 100%	Distillate 100%	Distillate 100%
CTG triet Air Cooling	Evap. Conter	Off	Off	Off	Off	Off
CTG SteamAVater Injection Ambient Temperature, F	Water 59	Water 59	Water 59	No. 100	Water 100	Water 100
HRSG Dutt Firing Fuel Sulfur Content (grains/100 standard cubic feet)	Unfired 568.31	Unfired 586.31	Unfired 568.31	Unfired 2.00	Unfired 568.31	Fired 568.31
Ambient Conditions	300.31)	300 011	300.01)			
Ambient Temperature, F Ambient Relative Humidity, %	59.0 60.0	59.0 60.0	. 59.0 60.0	100.0 48.4	100.0 48.4	100 0 48.4
Atmospheric Pressure, psia	14.690	14.690	14.690	14.690	14.690	14.690
Combustion Turbine Performance						
CTG Performance Reference	GTP	GTP	GTP	GTP	GTP	GTP
CTG Inlet Air Conditioning Effectiveness, %	85		0		0	- 0
CTG Compressor Inlet Dry Butb Temperature, F	52.6 92.9	59.0	59.0	100.0 48.5	100.0 48.5	100.0 48.5
CTG Compr. Inlet Relative Humidity, %		60.2	60.2			
Inlet Loss, in. H2O Exhaust Loss, in. H2O	13.2	13.2	4.0 13.2	4.0 13.2	4.0 13.2	4.0 13.2
CTG Load Level (percent of Base Load) Gross CTG Output, NW	182,000	75% 134,700	50% 89,800	100% 144,600	100% 154,800	100% 154,800
Gross CTG Heat Rate, Blu/kWh (LHV)	10,120	10,980	12,960	9,835	10,480	10,480
Gross CTG Heet Rate, Btu/nWh (HHV)	10,778	11,694	13,802	10,910	11,161	11,161
CTG Heat Input, MBtu/n (LHV)	1,841.8	1,479.0	1,153.8	1,422.1	1,622.3	1,622.3
CTG Heat input, MBlu/h (HHV)	1,961.8	1,575.2	1,239.5	1,577.5	1,727.8	1,727.8
CTG Water/Steam Injection Flow, Ib/h Injection Fluid/Fuel Ratio	135,030	100,920	71,150 1.1	0.0	108,580	108,580
CTG Exhaust Frow, Brh CTG Exhaust Temperature, F	3,806,000 1,092	2,992,000 1,159	2,458,000 1,200	3,235,000 1,163	3,359,000 1,151	3,359,000 1,151
Combustion Turbine First						
Total CTG Fuel Flow, fb/h	100,550	80,820	53,600	68,320	88,650	88,650
CTG Fuel Temperature, F	50		60	365	60	60
CTG Fuel LHV, Btu/fb CTG Fuel HHV, Btu/fb	18,300 19,490	18,300 19,490	18,300 19,490	20,816 23,091	18,300 19,490	18,300 19,490
HHV/LHV Ratio	1.0650	1.0650	1.0650	1.1093	1.0850	1.0850
CTG Fuel Composition (Ultimate Analysis by Weight)						
	0.00% 85.00%	0.00%	0.00% 85.00%	0.00% 73.76%	0.00% 85.00%	0.00% 85.00%
H2 N2	14.80%	14.80% 0.20%	14.80%	24.01% 0.61%	14.80% 0.20%	14.80%
02	0.00%	0.00%	0.00%	1,61%	0.00%	0,00%
S Total	0.00150%	0.00150% 100.00%	0.00150%	0.00657%	0.00150%	0.00150%
Fuel Suttur Content (greins/100 standard cubic feel)	566.31	566,31	566.31	2.00	566.31	588.31
Combustion Turbina Exhaust						
CTG Exhaust Analysis (Volume Basis - Wet)	12,000					
	0.89%	0.89% 5.40%	0.90% 5.19%	0.91%	0.88% 5.24%	0.88% 5.24%
H2O N2	12.17% 70.67%	11.83% 70.99%	10.88% 71.64%	10.14% 72.86%	13.39% 69.71%	13.39% 69.71%
02	11.00%	10.90%	11.39%	12.42%	10.79%	10.79%
SO2, (after SO2 oxidation) SO3, (after SO2 oxidation)	0.00003%	0.00003%	0.00003%	0.00010% 0.00002%	0.00003%	0.00003% 0.00001%
Total	100.0%			100.0%	100.0%	100.0%
Molecular WI, Ib/mol	28.19	28.24	28.32	28.19	28.05	28.06
Specific Volume, (1°3/fb Specific Volume, sct/fb	38.94 13.46	40.55 13.44	41.45 13.40		40.62 13.53	40.62 13.53
Exhaust Gas Flow, acfm Exhaust Gas Flow, acfm	2,470,094 853,813	2,022,093 670,208	1,696,478 548,953	2,195,487 725,718	2,274,043 757,455	2,274,043 757,455
CTG NOx Emissions (Without Post Combustion Emissions Control)	X San				7.07	151,140
Additional Percent Margin included in mass based NOx Emissions below	0%	0%	0%	0%	0%	0%
NOx, pprind (dry, 15% O2)	42.00	42.00	42.00	9.00	42.00	42.00
NOx, ppmvd (dry) NOx, ppmvv (wet)	59.40 52.20	50.50 53.40	57.50	10.80 9.70	59.80 51.80	59.80 51.80
NOx, Ibrh as NO2	325.5	261.6	206.2	52.5	286.9	286.9
NOx, toMBtu (HV) NOx, toMBtu (HV)	0.1767 0.1659	0.1769 0.1661	0.1772 0.1664	0.0369	0.1768 0.1660	0.1768 0.1660
CTG CO Emissions (Without Point Combustion Emissions Control)	\$\$0.27%@\$75,\$\$\$\$\$\$		1070 P.O. (1000 X. 2013)	6218000000000000000000000000000000000000		
Additional Percent Margin included in mass based CO Emissions below	0%	0%				09
CO, ppmvd (dry, 15% O2)	14,10	13.90	14.60	7.50	14.00	14.00
CO, ppmwd (dny) CO, ppmww (wet)	20.00 17.60	20.00	20.00 17.80	9.00 8.10	20.00 17.30	20.00 17.30
CO, the/h	66.5	52.5	43.5	26.1	58.2	58.2
CO, Io/MBtu (LHV) CO, Io/MBtu (HHV)	0.0361 0.0339	0.0355 0.0333	0.0374 0.0351	0.0184 0.0166	0,0359 0.0337	0.0359 0.0337
CTG SO2 Emissions (After 802 Daydistion, William Post Combustion Emissions Control)		4450 100 100 100	The second	er transmission		
Additional Percent Margin included in Ib/n SO2 Emissions below	0.0%	0.0%	0.0%	0.0%	0.0%	0.09
Assumed SO2 oxidation rate in CTG, vol%	20.0%	20.0%	20.0%	20.0%	20.0%	20.09
SO2, pprivd (dry, 15% O2) SO2, pprivd (dry)	0.2247 0.3177	0.2247 0.3238		0.9083	0.2247 0.3199	D.2247 0.3199
SO2, ppmww (wet)	0.2790	0.2855	0.2743	0.9760	0.2771	0.2771
SO2, Ib/h SO2, Ib/MBIU (LHV)	2.4133 0.0013					2.1256 0.0013
SO2, Ib/MBtu (HHV)	0.0012					0.0012
				1		

1/14/2005						
FMPA						
Tressure Coast Energy Center Unit 1 Black & Vestch Project 13855.0030						
1x1 Emissions Estimates						
Case Number	60	61	62	63	64	65
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG724
CTG Fuel Type	Distillate	Distiflate	Distillate	Natural Gas	Distillate	Distillat
CTG Load	100%	75%	50%	100%	100%	1009
CTG tritel Air Cooling	Evap. Cooler	Off	Off	Off	Off	0
CTG Steam/Water Injection	Water	Water 59	Water	No	Water	Wat
Ambient Temperature, F HRSG Duct Firing	59 Unfred	59 Unfired	59 Unfired	100 Unfired	100 Unfired	10 Fire
Fuel Sulfur Content (grains/100 standard cubic feet)	566.31	568.31	566.31	2.00	566.31	566.3
Combustion Turbine Exhaust - continued	· · · · · · · · · · · · · · · · · · ·					
CTG UNIC Emissions (Without Post Combustion Emissions Control)	0.0%	70-60-60-60-00-00-00-00-00-00-00-00-00-00	00%	0.0%	0.00	0.0
Additional Percent Margin included in Io/h UHC Emissions Below	0.0%	0.0%	00%	0.0%	0.0%	0,0
UHC, pprmvd (dry, 15% O2)	56	5.5	5.7	6.5	5.7	5.1
UHC, pprivd (dry)	80	7.9	7.9	7.8	8.1	8.
UHC, ppm/w (wet)	7.0	7.0	7.0	7.0	7.0	7.
UHC, fb/h as CH4	15.2	11.9	9.7	12.9	13.4	13.
UHC, Is/MBtu as CH4 (LHV)  UHC, Is/MBtu as CH4 (HHV)	0.0082	0.0080	0.0084	0.0091	0.0083	0.008
Unic, liximoliu as Ch4 (nn4)	0.0077	0.0070	0.0019	0.0002	0.0078	0.007
CTG YOC Emissions (Without Post Combustion Estissions Control)	WATER THE THE PROPERTY OF		-RY: 1884-01955	2500 2000 2000 CE	0.000	<b>\$</b> \$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$
Additional percent margin included in Ibin VOC emissions below	0%	0%	0%	0%	0%	0
<u> </u>						
VOC percentage of UHC	50%	50%	50%	20%	50%	50
VOC, ppmvd (dry, 15% O2)	2.8	2.8 4.0	2.9	1.3	2.B	2.
VOC, ppmw (wet)	3.5	3.5	3.5	1.4	3.5	3.
VOC, In/n as CH4	7.6	5.9	4.9	2.6	6.7	6.
VOC, Ib/MBtu as CH4 (LHV)	0.0041	0.0040	0.0042	0.0018	0.0041	0.004
VOC, Ib/MBitu as CH4 (HHV)	0.0039	0.0038	0.0039	0.0016	0.0039	0.003
CTG PM19 Emissions (without the Effects of SC2 Oxidation)	Proc. of a 7 Land Basic Confederation of the Confederation			690-2000 1255 1947 V		
Percent margin included in PM10 emissions below	0%	0%	0%	0%	0%	0
Perceix marger sections of PMTO diffusioning person	1					•
PM10 Emissions - Front Half Catch Only						
PM10, tb/h	17.0	17.0	17.0	9.0	17.0	17.0
PM10, Ib/M8tu (LHV)	0.0092	0 0115	0.0146	0.0063	0.0105	0.0105
PM10, IDMBtu (HHV)	0.0087	0.0108	0.0137	0.0057	0.0098	0.0096
PM10 Emissions - Front and Back Half Catch						
PM10, b/h	34.0	34.0	34.0	18.0	34.0	34.0
PM10, Ib/MBIu (LHV)	0.0185	0.0230	0 0292	0.0127	0.0210	0.021
PM10, tb/MBtu (HHV)	0.0173	0.0216	0 0274	0.0114	0.0197	0.0197
				I		
HRSG Duct Burners						
HRSG Duct Burners			SWEBSCOX, G-Cress	<b>3325</b> 45574574873		
Duct Burner Heat Input, MBruth (LHY)	0.0	0.0	0.0	0.0	0.0	485
Duct Burner Heat Input, MBNuh (LHV) Duct Burner Heat Input, MBNuh (LHV) Duct Burner Heat Input, MBNuh (HHV)	0.0	0.0	0.0	0.0	0.0	485. 538.
Duct Burner Heat Input, MBruth (LHY)	0.0	0.0	0.0	0.0	0.0	485
Diad Burner Fuel  Duct Burner Heel Input, MBtu/h (LHV)  Duct Burner Heel Input, MBtu/h (HHV)	0.0	0.0	0.0	0.0	0.0	485 538
Duct Burner Fuel Plow, MBtu/n (LHV) Duct Burner Heat Input, MBtu/n (LHV) Total Duct Burner Fuel Flow, Ibrh	0.0	0.0	0.0	0.0	0.0	495 538 23,30
Diad Burner Fuel  Duct Burner Heel Input, MBtu/h (LHV)  Duct Burner Heel Input, MBtu/h (HHV)	00	0.0 0.0 0	0.0 0.0 0	00	0.0 0.0 0	485 538
Duct Burner Fuel Pow, MButh (LHV) Duct Burner Heal Input, MButh (HHV) Total Duct Burner Fuel Flow, Ibth  Duct Burner Fuel LHV, Sturtb Duct Burner Fuel HHV, Sturtb Duct Burner Fuel HHV, Sturtb	00 0.0 0 20,816	0.0 0.0 0	0.0 0.0 0	0.0 0.0 0	0.0 0.0 0	485 538 23,30 20,81
Duct Burner Fuel Input, MBIUM (LHV) Duct Burner Heat Input, MBIUM (LHV) Total Duct Burner Fuel Flow, IbM  Duct Burner Fuel LHV, BIUM Duct Burner Fuel HHV, BIUM Duct Burner Fuel HHV, BIUM Duct Burner Fuel HHV, BIUM Duct Burner Fuel Composition (Ultimate Analysis by Weight)	20.815 23.091	0.0 0.0 0 20,815 23,091	0.0 0.0 0 20,816 23,091	0.0 0.0 0 20,816 23,091	0.0 0.0 0 20,816 23,091	465 538 23,30 20,81 23,00
Duct Burner Feel Input, MBIUM (LHV) Duct Burner Heel Input, MBIUM (HHV) Total Duct Burner Heel Flow, IbM Duct Burner Fuel Flow, IbM Duct Burner Fuel HHV, Blutb Duct Burner Fuel HHV, Blutb Duct Burner Fuel Composition (Ultimate Analysis by Weight) At	20.815 23.091	0.0 0.0 0 20,815 23,091	0.0 0.0 0 20,816 23,091	20,816 23,091	20,816 23,091	495 538 23,8 20,8 23,00
Duct Burner Fuel Input, MBIUM (LHV) Duct Burner Heat Input, MBIUM (LHV) Total Duct Burner Fuel Flow, IbM  Duct Burner Fuel LHV, BIUM Duct Burner Fuel HHV, BIUM Duct Burner Fuel Composition (Utilimate Analysis by Weight) Ar C	20.815 23.091	0.0 0.0 0 20,815 23,091	0.0 0.0 0 20,816 23,091	0.0 0.0 0 20,816 23,091	20,816 22,981 20,091	485 538 23,8 20,8 20,8 73,7
Duct Burner Feel Input, MBIUM (LHV) Duct Burner Heel Input, MBIUM (HHV) Total Duct Burner Heel Flow, IbM Duct Burner Fuel Flow, IbM Duct Burner Fuel HHV, Blutb Duct Burner Fuel HHV, Blutb Duct Burner Fuel Composition (Ultimate Analysis by Weight) At	20,816 23,091 0 0 0 0 0 0 0 0 0 73,76%	20,815 23,981 20,00%	20.816 22.091 0 00%	00 00 0 20,816 23,091 0,00%	20,816 23,091	455 538 23,5 20,8 23,5 0.00 7377 240
Duct Burner Fuel Input, MBuuh (LHV) Duct Burner Heat Input, MBuuh (LHV) Total Duct Burner Fuel Flow, Buh  Duct Burner Fuel Flow, Buh  Duct Burner Fuel HHV, Blu/Ib  Duct Burner Fuel Composition (URmate Analysis by Weight)  Ar  C  H2  N2  O2	0.00 0.00 20.815 23.091 0.0004, 73.78%, 24.01%, 0.61%	0.0 0.0 0 20.815 23.091 0.00% 73.76% 24.01% 0.01%	00 00 0 0 20,816 23,091 0,00% 73,76% 24,01% 0,61%	00 00 0 0 20,816 23,091 0,00% 73,78% 24,01% 0,61%	0.0 0.0 0 0 20.816 23.091 0.00% 73.76% 24.01% 0.61%	20,8 22,8 23,8 23,8 20,0 20,0 20,0 21,2 24,0 24,0 26,0 18,0
Duct Burner Fuel Pow, MButh (LHV) Duct Burner Heel Input, MButh (LHV) Total Duct Burner Fuel Flow, Ibth  Duct Burner Fuel LHV, Blufb Duct Burner Fuel HHV, Blufb Duct Burner Fuel HHV, Blufb Duct Burner Fuel Composition (Ul	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0 20.816 23.091 0.00% 73.79% 24.01% 0.015%	0.0 0.0 0.0 20.816 23.091 0.00% 73.78% 24.01% 0.61% 0.00557%	00 00 0 20 516 23 091 0 00% 73 75 75% 24 01% 0 615%	0.0 0.0 0 20.816 23.091 0.00% 7.3.79% 24.01% 0.01%	485 530 23,8 20,8 20,8 20,0 0,0 0,0 0,0 0,0 0,0
Duct Burner Fuel Pow, MButh (LHV) Duct Burner Heat Input, MButh (LHV) Total Duct Burner Fuel Flow, Ibth  Duct Burner Fuel LHV, Bluffb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 N2 C2 S Total	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0 0 20,815 23,091 0.00% 73,76% 24,01% 0.006%	0.0 0.0 0.0 20.816 22.091 0.00% 73.75% 24.01% 0.00657% 0.00657%	0.0 0.0 0.0 20.016 23.001 0.005 7.3 75% 24.01% 0.015% 1.161% 0.00057%	0.0 0.0 0.0 20.816 22.091 0.00% 73.70% 24.01% 0.01% 1.61%	455 533 23,3 23,3 23,0 0,00 7,3,7 24,0 0,00 1,5 0,000 1,000
Duct Burner Fuel Prov. (MBru/n (LHV) Duct Burner Heat Input, MBru/n (LHV) Total Duct Burner Fuel Flow, Ibr/n Duct Burner Fuel Flow, Ibr/n Duct Burner Fuel HTV, Bru/fb Duct Burner Fuel HTV, Bru/fb Duct Burner Fuel HTV, Bru/fb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 N2 C2 S	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0 20.816 23.091 0.00% 73.79% 24.01% 0.015%	0.0 0.0 0.0 20.816 23.091 0.00% 73.78% 24.01% 0.61% 0.00557%	0.0 0.0 0.0 20.016 23.001 0.005 7.3 75% 24.01% 0.015% 1.161% 0.00057%	0.0 0.0 0 20.816 23.091 0.00% 7.3.79% 24.01% 0.01%	453 533 23,35 22,35 22,05 22,05 22,05 24,01 0.05 1.05 1.05 1.00 1.00 1.00 1.00 1.
Duct Burner Fuel Input, MBIUM (LHV) Duct Burner Heal Input, MBIUM (LHV) Duct Burner Heal Input, MBIUM (HHV) Total Duct Burner Fuel Flow, IbM  Duct Burner Fuel LHV, Biu/Ib Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C HZ N2 C2 S Total Fuel Surfur Content (grainer/100 standard cubic feet)	0.0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0.0 0.0 0 0 20,815 23,091 0.00% 73,76% 24,01% 0.006%	0.0 0.0 0.0 20.816 22.091 0.00% 73.75% 24.01% 0.00657% 0.00657%	0.0 0.0 0.0 20.016 23.001 0.005 7.3 75% 24.01% 0.015% 1.161% 0.00057%	0.0 0.0 0.0 20.816 22.091 0.00% 73.70% 24.01% 0.01% 1.61%	455 533 23,3 23,3 23,0 0,00 7,3,7 24,0 0,00 1,5 0,000 1,000
Duct Burner Fuel Input, MBluh (LHV) Duct Burner Heal Input, MBluh (LHV) Duct Burner Heal Input, MBluh (HHV) Total Duct Burner Fuel Flow, Ibih  Duct Burner Fuel HVI, Blufb Duct Burner Fuel HVI, Blufb Duct Burner Fuel Composition (U8/mete Analysis by Weight) Ar C H2 N2 C2 S Total Fuel Suther Content (grainer/100 standard cubic feet)  Duct Burner Entestations (School (LHV))	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0 20.816 23.091 0.00% 73.79% 24.01% 0.015% 1.61% 1.00% 10.00%	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	00 00 00 20 816 23 091 0 00% 73 758 24 01% 0 01% 1 161% 1 000% 2 000 2 0000 2 000 2 000 2 000 2 0000 2 0000 2 000 2 000 2 000 2 000 2 000 2 000	0.0 0.0 0.0 20.816 23.091 0.00% 7.3.79% 24.01% 0.0957% 1.61% 1.00% 2.00	20,81 23,85 23,85 23,95 23,07 24,07 24,07 24,07 16,18 16,18 20,005 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,007 20,00
Duct Burner Feel Input, MBsuh (IHHY) Duct Burner Heal Input, MBsuh (IHHY) Duct Burner Heal Input, MBsuh (IHHY) Total Duct Burner Fuel Flow, Brh  Duct Burner Fuel HHV, Bsuhb Duct Burner Fuel HHV, Bsuhb Duct Burner Fuel Composition (Ultimate Analysis by Wetgitt) Ar C HZ NZ C S Total Fuel Suther Content (grainer/100 standard cubic feet)  Duct Burner Endesdoes (Fig. 16 Fig. 17 Fig. 1	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0 20.815 23.091 0.00% 73.79% 24.01% 0.01% 1.01% 0.00857% 1.01% 0.00857%	0.0 0.0 0.0 20.816 23.091 0.0057** 24.01% 0.0057** 1.01% 0.0057** 0.0057** 0.0050**	0.0 0.0 0.0 20.816 23.091 0.0056 7.3 785 24.01% 0.00577 1.01% 0.00577 1.01% 0.00577 0.00577	0.0 0.0 0.0 20.816 23.091 0.00% 73.78% 24.01% 0.00957% 1.01% 0.00957% 1.01% 0.00957%	20,8 22,8 23,8 23,8 23,0 0,000 23,7 24,0 0,000 100 0,000
Duct Burner Field Input, MBIUM (LHV) Duct Burner Heal Input, MBIUM (LHV) Total Duct Burner Heal Input, MBIUM (HHV) Total Duct Burner Fuel LHV, Bluftb Duct Burner Fuel LHV, Bluftb Duct Burner Fuel LHV, Bluftb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 H2 H2 O2 S Total Fuel Surfar Content (grains/100 standard cubic feet) Duct Burner Enalsdons #200 STAND (Library Burner) Duct Burner Enalsdons #200 STAND (Library Burner) Duct Burner Co, IbMBIU (HHV) Duct Burner LOC (Library Burner) Duct Burner CO, IbMBIU (HHV) Duct Burner LOC (Library Burner) Duct Burner LOC (Library Burner) Duct Burner HO2 (Library Burner) Duct Burner HO3 (Library Burner) Duct Burner HO4 (Library Burner)	0.00 0.00 20.818 23.091 23.091 0.00% 73.78% 0.00% 1.00% 0.00657% 1.00% 0.0060 0.0060 0.0060 0.0060 0.0060	0.0 0.0 0.0 20.816 23.091 0.00% 7.3 78% 24.01% 0.61% 1.00% 1.00057% 100.0% 2.000	0.0 0.0 0.0 20.816 23.091 0.00% 7.3 76% 24.01% 0.00857% 100.00% 2.00 0.000 0.000	00 00 00 20 816 23 091 000% 73 78% 24 01% 0 00057% 100 00057% 0 000057% 0 0000 0 0000 0 0000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	485 530 23,3 20,8; 23,9 20,0 73,7,7 240 9 8 1,0 2,0 100 2,0 0,0 0,0 0,0
Duct Burner Feel Irput, MBbuth (LHV) Duct Burner Heal Irput, MBbuth (LHV) Duct Burner Heal Irput, MBbuth (HHV) Total Duct Burner Fuel Flow, Ish Duct Burner Fuel HV, Bbuth Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C C H2 N2 C2 S Total Fuel Suther Content (grainer/100 standard cubic feet)  Duct Burner Entestions (** 15 % 15 % 15 % 15 % 15 % 15 % 15 % 15	0.00 0.00 20.815 23.091 0.000 7.37 F5% 24.01% 0.00557% 1.00 0% 0.000 0.000 0.000 0.000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 20.016 22.091 0.0057 73.76% 24.01% 0.0057% 1.01% 0.0057% 0.000 0.000 0.000 0.000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	455 533 23,3 23,3 23,3 23,0 0,00 7,3,7 24,0 0,0 1,0 1,0 1,0 1,0 1,0 1,0 1
Duct Burner Fuel Input, MBsuhr (LHV) Duct Burner Heel Input, MBsuhr (LHV) Total Duct Burner Fuel Flow, IbNh Total Duct Burner Fuel LHV, Bsuhb Duct Burner Fuel LHV, Bsuhb Duct Burner Fuel Composition (URImate Analysis by Weight) Ar C H2 N2 O2 S Total Duct Burner Fuel Composition (URImate Analysis by Weight) Duct Burner Fuel Composition (URImate Analysis by Weight) Ar C Duct Burner Fuel Composition (URImate Analysis by Weight) Ar C Duct Burner Fuel Composition (URImate Analysis by Weight) Duct Burner Fuel Subhibation (URImate Analysis by Weight) Duct Burner Fuel Subhibation (URImate Analysis by Weight) Duct Burner Fuel Subhibation (URImate Analysis by Weight) Duct Burner HVD, Bahffelly (HHV) Duct Burner HVD, (as CH4), Bahffelly (HHV) Duct Burner VDC (as CH4), Bahffelly (HHV)	0.00 0.00 20.818 23.091 23.091 0.00% 73.78% 0.00% 1.61% 0.00657% 1.00% 0.000 0.000 0.000 0.000 0.000 0.000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 20.816 22.091  0.00% 73.78% 24.01% 0.00% 73.70% 2.00 0.00% 0.00% 0.00% 0.00%	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	455 538 22,35 20,81 23,08 20,81 23,08 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0
Duct Burner Feel Irput, MBbuth (LHV) Duct Burner Heal Irput, MBbuth (LHV) Duct Burner Heal Irput, MBbuth (HHV) Total Duct Burner Fuel Flow, Ish Duct Burner Fuel HV, Bbuth Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C C H2 N2 C2 S Total Fuel Suther Content (grainer/100 standard cubic feet)  Duct Burner Entestions (** 15 % 15 % 15 % 15 % 15 % 15 % 15 % 15	0.00 0.00 20.815 23.091 0.000 7.37 F5% 24.01% 0.00557% 1.00 0% 0.000 0.000 0.000 0.000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 20.016 22.091 0.0057 73.76% 24.01% 0.0057% 1.01% 0.0057% 0.000 0.000 0.000 0.000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	000 000 000 000 000 000 000 000 000 00
Duct Burner Fuel Input, MBsuhr (LHV) Duct Burner Heel Input, MBsuhr (LHV) Total Duct Burner Fuel Flow, IbNh Total Duct Burner Fuel LHV, Bsuhb Duct Burner Fuel LHV, Bsuhb Duct Burner Fuel Composition (URImate Analysis by Weight) Ar C H2 N2 O2 S Total Duct Burner Fuel Composition (URImate Analysis by Weight) Duct Burner Fuel Composition (URImate Analysis by Weight) Ar C Duct Burner Fuel Composition (URImate Analysis by Weight) Ar C Duct Burner Fuel Composition (URImate Analysis by Weight) Duct Burner Fuel Subhibation (URImate Analysis by Weight) Duct Burner Fuel Subhibation (URImate Analysis by Weight) Duct Burner Fuel Subhibation (URImate Analysis by Weight) Duct Burner HVD, Bahffelly (HHV) Duct Burner HVD, (as CH4), Bahffelly (HHV) Duct Burner VDC (as CH4), Bahffelly (HHV)	0.00 0.00 20.818 23.091 23.091 0.00% 73.78% 0.00% 1.61% 0.00657% 1.00% 0.000 0.000 0.000 0.000 0.000 0.000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 20.816 22.091  0.00% 73.78% 24.01% 0.00% 73.70% 2.00 0.00% 0.00% 0.00% 0.00%	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	20,8 23,9 23,9 23,0 23,0 23,0 23,0 24,0 24,0 25,0 26,0 27,0 27,0 27,0 28,0 28,0 28,0 28,0 28,0 28,0 28,0 28
Duct Burner Feel Input, MBsuhr (LHV) Duct Burner Heel Input, MBsuhr (LHV) Total Duct Burner Feel Flow, Birth Total Duct Burner Feel Flow, Birth Duct Burner Feel Flow, Birth Duct Burner Feel LHV, Blurth Duct Burner Feel Composition (Ultimate Analysis by Weight) Ar C H2 N2 C2 S Total Feel Surtur Content (grains/100 standard cubic feet) Duct Burner For Content (grains/100 standard cubic feet) Duct Burner MD, BMBbs (HHV) Duct Burner MCC (as CHA) BMBbs (HHV) Duct Burner VHC (as CHA) BMBbs (HHV) Duct Burner VHC (as CHA) BMBbs (HHV) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only) Duct Burner FM10, BMBbs (HHV) (front half catch only)	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.00 0.00 20.816 23.091  0.00% 73.76% 24.01% 0.00% 10.00% 0.000 0.000 0.000 0.000 0.000 0.000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	20,8 23,3 23,0 20,0 23,0 23,0 23,0 24,0 24,0 24,0 25,0 26,0 26,0 26,0 26,0 26,0 26,0 26,0 26
Duct Burner Fuel Input, MBIUM (LHV) Duct Burner Heal Input, MBIUM (LHV) Total Duct Burner Fuel Flow, Ibsh  Duct Burner Fuel LHV, Sturb  Duct Burner Fuel HHV, But/b  Duct Burner Fuel Composition (U8/mate Analysis by Weight)  Ar  C  H2  N2  O2  S  Total  Fuel Subtract Content (grainer/100 standard cubic feet)  Duct Burner Entistations (MBIUM (HHV) Duct Burner CD, IbshBib (HHV) Duct Burner CD, IbshBib (HHV) Duct Burner VDC (as CH4), IbshBib (HHV) Assumed SO2 addition rate in Duct Burner, voffs	0.0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.004 7.3 795 24.015 0.0957 1.0574 1.0574 0.00507 0.000 0.000 0.000 0.000 0.000	20,8 23,3 23,3 23,0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0
Duct Burner Feel Input, MBsuh (IHV) Duct Burner Heel Input, MBsuh (IHV) Total Duct Burner Fuel Input, MBsuh (IHV) Total Duct Burner Fuel Input, MBsuh (IHV) Duct Burner Fuel Input, Bsuhb Duct Burner Fuel Input, Bsuhb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C HZ N2 O2 S Total Fuel Suther Content (grains/100 standard cubic feet)  Duct Burner Fuel NO, IbMBsu (HV) Duct Burner Fuel Composition (Ultimate Analysis by Weight) Duct Burner HOC, IbMBsu (HV) Duct Burner HOC, IbMBsu (HV) Duct Burner PMIO, IbMBsu (HVI) Duct Burner PMIO, IbMBsu (HVI) (foot and back half catch) Duct Burner PMIO, IbMBsu (HVI) (foot and back half catch) Assumed SO2 oxidation rate in Duct Burner voffs Total SO3, Ibh from Duct Burner Fuel only (after SO2 oxidation) Total SO3, Ibh from Duct Burner Fuel only (after SO2 oxidation) Total SO3, Ibh from Duct Burner Fuel only (after SO2 oxidation)	0.0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	20,81 22,32 23,32 23,32 23,02 23,02 24,02 24,02 25,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02 20,02
Duct Burner Fuel Input, MBsuhr (LHV) Duct Burner Heel Input, MBsuhr (LHV) Total Duct Burner Fuel Input, MBsuhr (HHV) Total Duct Burner Fuel Input, MBsuhr (HHV) Duct Burner Fuel LHV, Bsuhrb Duct Burner Fuel Composition (URimate Analysis by Weight) Ar C H2 N2 O2 S Total Duct Burner Fuel Composition (URimate Analysis by Weight) Duct Burner Fuel Composition (URimate Analysis by Weight) Ar C H2 N2 O2 S Total Duct Burner Fuel Composition (URimate Analysis by Weight) Duct Burner Holl (grainer/100 standard cubic feet) Duct Burner Holl (grainer/100 standard cubic feet) Duct Burner HOL, BAMBsu (HHV) Duct Burner HOL (ga CH4), BaMBsu (HHV) Duct Burner HOL (ga CH4), BaMBsu (HHV) Duct Burner HOL (ga CH4), BaMBsu (HHV) Duct Burner PM10, BMBsu (HHV) (fort and fact on hy) Duct Burner PM10, BMBsu (HHV) (fort and back half catch only) Duct Burner PM10, BMBsu (HHV) (fort and back half catch) Assumed SO2 addition rate in Duct Burner , voffix Total SO2, Boh from Duct Burner Fuel only (after SO2 addition) DB NOs, Boh	0.00 0.00 20.818 23.091 23.091 0.00% 73.78% 0.00% 13.16% 0.00% 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	20,81 23,85 23,85 23,95 23,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 24,07 26,07 26,07 26,07 26,07 26,07 26,07 26,07 26,07 26,07 26,07 26,07
Duct Burner Feet Input, MBsuh (LHV) Duct Burner Heet Input, MBsuh (LHV) Total Duct Burner Feet Input, MBsuh (HHV) Total Duct Burner Feet Input, MBsuh (HHV) Total Duct Burner Feet Input, Bsuhb Duct Burner Feet LHV, Bsuhb Duct Burner Feet Composition (Ultimate Analysis by Weight) Ar C H2 N2 O2 S Total Fuet Suther Content (grains/100) standard cubic feet) Duct Burner Endasdoria (Schiller Herb) Duct Burner MCN, (MMBsu (HHV) Duct Burner CC (sac CHA) (MMBsu (HHV) Duct Burner PMIO, (MMBsu (HHV) (foort and back half catch) Assumed SO2 addation rate in Duct Burner vid [®] Total SO2, Bsh from Duct Burner Fuet only (after SO2 addation) Total SO3, Bsh from Duct Burner Fuet only (after SO2 addation) DB NO1, Bsh	0.00 0.00 20.815 23.091 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.00 0.00 20.816 23.091 0.00577 77.76% 24.01% 0.00577 0.0000 0.000 0.000 0.000 0.000 0.000 0.000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	20,81 20,81 22,05 23,05 22,05 22,05 22,05 24,01 24,01 20,005 100 20,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00,000 00
Duct Burner Fuel Input, MBuuh (LHV) Duct Burner Heel Input, MBuuh (LHV) Total Duct Burner Fuel Input, MBuuh (HHV) Total Duct Burner Fuel Input, MBuuh (HHV) Duct Burner Fuel Inv. Baufb Duct Burner Fuel Composition (Ultimate Analysis by Weight) Ar C H2 N2 Q2 Q3 S Total Fuel Suther Content (grainer/100 standard cubic feet) Duct Burner Rot, BuMBbu (HHV) Duct Burner Fuel Burner (Input Burner) Duct Burner PMD, BuMBbu (HHV) Duct Burner VDC (as CH4) (buMBbu (HHV) Duct Burner VDC (as CH4) (buMBbu (HHV) Duct Burner PMD, BuMBbu (HHV) Duct Burner PMD, Burner Fuel only (after SO2 oxidation) Total SO3, Buh from Duct Burner Fuel only (after SO2 oxidation) DB NO1, Buh DB NO1, Buh DB NO2, Buh DB NO3, Buh DB NO4, Buh DB UNC (as CH4), Buh	0.00 0.00 20.818 23.091 23.091 0.00% 73.78% 0.00% 13.16% 0.00% 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0	20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81 20,81
Duct Burner Fleet Imput, MBsu/n (LHV) Duct Burner Heet Input, MBsu/n (LHV) Total Duct Burner Fleet Flow, Ibn Duct Burner Fleet Flow, Ibn Duct Burner Fleet Flow, Ibn Duct Burner Fleet Hew, Bsu/n Duct Burner Fleet Hew, Bsu/n Duct Burner Fleet Hew, Bsu/n Duct Burner Fleet Composition (Ultimate Analysis by Weight) Ar C H2 N2 C2 S Total Fleet Surfur Content (grains/100) standard cubic feet) Duct Burner Entesticitis (Schiller Fleet) Duct Burner Entesticitis (Schiller Fleet) Duct Burner Fleet Cap (LHW) Burlish (PHV) Duct Burner PMI (D, IbMBib (HHV) Duct Burner PMI (D, IbMBib (HHV) (forcit and back half catch) Duct Burner PMI (D, IbMBib (HHV) (forcit and back half catch) Duct Burner PMI (D, IbMBib (HHV) (forcit and back half catch) Total SO2, Bsh from Duct Burner Fleet only (after SO2 oxidation) Total SO3, Bsh from Duct Burner Fleet only (after SO2 oxidation) DB NO3, Bsh	0.00 0.00 20.816 23.091 0.00% 73.787% 0.00% 73.787% 10.00% 0.0067% 10.00% 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060 0.0060	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 20.816 23.091 0.005 73.7878 24.01% 0.005 10.005 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	455 538 23,30 20,81 22,06 0,00 73,76 24,01 0,01 1,91 1,91 1,91 1,91 1,91 1,91 1
Duct Burner Field   Market   Duct Burner Field   Market   Duct Burner Heat Input, MBButh (LHV) Duct Burner Heat Input, MBButh (LHV) Total Duct Burner Field   Flow, Ibrh  Duct Burner Field   HVV, (Burlib Duct Burner Field   HVV, (Burlib Duct Burner Field   Composition (Ultimate Analysis by Weight)  Ar  C  H2  N2  O2  S  Total Field Suther Content (grains/100 standard cubic feet)  Duct Burner Rob, IbrhButh (HVV) Duct Burner ROb, IbrhButh (HVV) Duct Burner ROC, IbrhButh (HVV) Duct Burner PMIO, IbrhButh (HVV) Total SO2, Ibrh from Duct Burner Field only (after SO2 oxidation)  Total SO2, Ibrh from Duct Burner Field only (after SO2 oxidation)  D8 NOs, Ibrh D8 DOC, Ibrh D8 UHC (as CH4), Ibrh D8 UHC (as CH4), Ibrh D8 UNC (as CH4), Ibrh D8 UNC (as CH4), Ibrh D8 UHC (as CH4), Ibrh D8 UNC (as CH4), Ibrh D8 UNC (as CH4), Ibrh	0.00 0.00 20.815 23.091 0.00% 7.3 76% 24.01% 0.00% 7.3 76% 100.0% 0.0000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	20,8 20,8 23,3 23,3 24,0 0,0 1,0 1,0 0,0 0,0 0,0 0,0 0,0 0,0 0

1/14/2006						
FMPA						
Treasure Coast Energy Center Unit 1 Black & Veetch Project 13859,0030						
1x1 Emissions Estimates						
Case Number	60	61	62	63	54	6
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PC
CTG Fuel Type	Distillate	Distillate	Distillate	Natural Gas	Distillate	Di
CTG Load	100%	75%	50%	100%	100%	
CTG triet Air Cooling	Evap. Cooler	Off	Off	Off	Off	
CTG SteamWater Injection	Water	Water	Water	No	Water	
Ambient Temperature, F	59	59	59	100	100	
HRSG Duct Firing	Unfired 568.31	Unfired 566 31	Unfired 566 31	Unfired 2.00	Unfired 566 31	
Fuel Sulfur Content (grains/100 standard cubic hel)	3031	360 31	300 311	200	500.31	TT
Stack Emissions						
Stack Exhaust Analysis - Vokene Basis - Wes		法的不同性的基础的支	DESCRIPTION OF THE	Action of the Control	5)490040666 06,000	<b>被心</b> 形态水池
Ar	0.89%	0.89%	0.90%	0.91%	0.88%	
CO2	5.28%	5 40%	5.19%	3 66%	5.24%	
H2O N2	12.17% 70.57%	11,83% 70,99%	10.88%	10.14% 72.86%	13.39% 69.71%	1 6
02	11.00%	10,90%	11.39%	72.56% 12.42%	10.79%	
SO2 (after SO2 oxidation)	0.000020%	0.000020%	0.000020%	0.000070%	0.000020%	0.00
SO3 (after SO2 oxidation)	0.000020%	0.000020%	0.000020%	0.000050%	0.000020%	0.00
Total	100.0%	100.0%	100.0%	100.0%	100.0%	1
Stack Exit Temperature, F	263	245			263	
Stack Diameter, ft (estimated)	18	18	18	18	18	
Stack Flow, Ib/h	3,805,999	2,991,999	2,457,999	3,234,997	3,358,999	3,38
Stack Flow, scrtm	853,813	670,208	548,953	725,718	757,455	76
Stack Flow, actm Stack Exit Velocity, fVs	1,188,106 78.0	909,089	742,726 49.0	895,556 59.0	1,053,047	1,04
SLIBCK EXIT VENCHITY, IVS	78.0	80.0	49.0	39.0	09,0	-
Stack NOs Emissions without the Effects of Selective Catalytic Reduction (SCR)	部の表の声がというな性であ	PT. 2008203467866790	COMPANYOR CHARGE TO	14.0% (F.3644.5863)	G997::0490(S):-1050(2006	PROGRAMME
NOx, sprind (dry, 15% O2)	42.0	420	42.0	9.0	42.0	
NOx, ppmvd (dry)	59.4	60.5	57.5	10.8	59.8	
NOx, pprinw (wet)	52.2	53.4	51.3	9.7	51.8	
NOx, forh as NO2 (includes correction adder)	325.5	261.6	206.2	52.5	286.9	
NOx, IbMBtu (LHV) as NO2 (Incl. duct burner fuel)	0.1767	0,1769	0.1772	0.0369	0.1768	
NOx, Ib/MBtu (HHV) as NO2 (incl. duct burner fuel)	0.1659	0.1561	0.1684	0 0333	0,1680	
Stack NOx Emissions with the Effects of Selective Catalytic Reduction (SCR)	を認めるのでものである。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表現しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 をません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しません。 を表しる。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をません。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん。 をもん	<b>然为</b> 的人们是一个社会的实现。	SAME AND A STREET OF THE SAME AND A	SELECTION OF SELECT	THE RESERVE OF THE PARTY OF THE	Realis to animal
NOx, ppmyd (dry, 15% O2)	8.0	8.0	8.0	2.0	8.0	
NOx, pprovd (dry)	11.3	11.5	11.0	2.4	11.4	
NOx, ppmww (wet)	99	10.2	98	2.1	9.9	
NOx, lb/h as NO2 (includes NOx margin applied to CTG)	62.0	49.8	39.3	11.7	54.6	ļ <u> </u>
NOx, b/MBtu (LHV) as NO2 (Incl. duct burner fuel)	0.0337	0.0337 0.0316	0.0338	0.0082	0.0337	
NOx, bMBbu (HHV) as NO2 (incl. duct burner fuel)	0.0316	0.0316	0.0317	0.0074	0.0316	
SCR NH3 slip, ppmvd (dry, 15% O2)	5.0	5.0	50	10.0	5.0	<del></del>
SCR NH3 slip, bith	14.3	11.5	9.0	21.0	12.6	
A Stack CO Entestion 不通過的影響。如此語彙是是一個的學術。不過,因此是一個的學術是一個學術的學術的學術。	82.20E1	CHANGE GRANK	SACAMETER AND	"24" DIF" (K. SORMA	PROCESSOR AND	1986#23 - A
CO, ppmvd (dry, 15% O2)	14.1	13.9	146	7.5	14.0	
CO, ppmvd (dry)	20.0	20.0		9.0	20.0	
CO, pprinwr (wet)	17.6	17.6	17.8	8.1	17.3	ļ <u> </u>
CO, Itsh. (includes CO margin applied to CTG)	66 6 0.0361	52.5 0.0355	43.5 0 0374	26.1	58.2	l
CO, Ib/MBtu (LHV) (Incl. duct burner fuel) CO, Ib/MBtu (HHV) (Incl. duct burner fuel)	0.0339	0.0333	0 03/4	0.0184	0.0359	
Stack SO2 Emissions, after SO2 Oxidation	_	(25/25/25/25/20/24)	CANADARINA AN S	JASSA SOSNIA SARRAS	SPENSAL SCHOOL	11800 a 1500 ;
Assumed SO2 axidation rate in CO Catalyst, vol%	20.0%		<del></del>			
Assumed SO2 audithon rate in CO Catalyst, vol% Assumed SO2 audition rate in SCR, vol%	3.0%	20.0%		20,0%	20.0%	
\$02, ppmvd (dry, 15% 02)	0.16	0.16	0.15		0.16	
SO2, ppmvd (dry)	0.22	0.23	0.21	0.76	0.22	
		0.20	0.19	0.68	0.19	
SO2, ppmwy (wet)	0.19					
SO2, pprmw (vet) SO2, lbMStu (LHV) (inct duct burner fuel)	1,69	1.35	1.07	5 01 0.0035	1.48 0.0009	ļ

i	1/14/2006	
ĺ	FMPA	
ı	Treasure Coast Energy Center Unit 1	
H	Black & Veatch Project 138869,0030	
į	1x1 Emissions Estimates	
ĺ	Case Number	
H	CTG Model	
H	CTG Fuel Type	
Н		

Case Number	60	61	62	63	64	65
CTG Model	PG7241	PG7241	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type	Distillate	Distillate	Distrilate	Natural Gas	Distillate	Distillate
CTG Load	100%	75%	50%	100%	100%	100%
CTG triet Air Cooling	Evap. Cooler	Off	Off	Off	Off	Off
CTG Steam/Water Injection	Water	Water	Water	No	Water	Water
Ambient Temperature, F	59	59	59	100	100	100
HRSG Duct Firing	Unfired	Unfired	Unfired	Unfired	Unfired	Fired
Fuel Sulfur Content (grains/100 standard cubic feet)	568.31	566.31	566.31	200	588.31	568.31
					-	

Start	<b>Francisco</b>	<ul> <li>continued</li> </ul>

Stack UHC Emissions	3.35.37.78.35.35.35.	AMMEDISTR MAY 1995	1788C/558698543		7379036360000000000	355/03880723800
UHC, ppmvd (dry, 15% O2)	5.6	5.5	5.7	6.5	5.7	15.0
UHC, ppmvd	8.0	7.9	7.9	7.8	8.1	27.9
UHC, ppmww	7.0	7.0	7.0	7.0	7.0	23.5
UHC, bt/h as CH4 (includes correction adder)	15.2	11.9	9.7	12.9	13.4	45.7
UHC, Ib/MBtu (LHV) (Incl. duct burner fuel)	0.0082	0.0080	0.0084	0.0091	0.0083	0.0217
UHC, Ib/MBtu (HHV) (Incl. duct burner fuel)	0,0077	0.0076	0.0079	0.0082	0 0078	0.0202
Stack VOC Emissions	0.0000000000000000000000000000000000000	1210 March 2010 F 100	.8024-63, 501 2-698.			
VOC, porrivd (dry, 15% O2)	2.8	2,8	2.9	1.3	2.8	29
VOC, ppmvd (dry)	4.0	4.0	39	1.6	4.0	5.4
VOC, ppmww (wet)	3.5	35	35	1.4	3.5	4.6
VOC, b/h as CH4 (Includes VOC correction as applied to CTG)	7.6	5.9	4.9	2.6	6.7	8.9
VOC, bt/MBtu (LHV) (incl. duct burner fuel)	0,0041	0.0040	0.0042	0.0018	0.0041	0.0042
VOC, ID/MBtu (HHV) (incl. duct burner fuel)	0.0039	0.0038	0.0039	0.0016	0.0039	0,0039
PRI 10 without the Effects of 602 oxidetion	Same and the second	SINKE A LOSSIA RENTE	SACRATION SECURE	-10		1 To
PM 10 Emissions - Front Half Catch Only						-
PM10, 8xh	17.0	17.0	17.0	9.0	17.0	22.4
PM10, Ib/MBtu (LHV) (incl. duct burner fuel)	0.0092	0.0115	0.0146	0.0063	0.0105	0.0108
PM10, lb/M8tu (HHV) (Incl. duct burner fuel)	0.0087	0.0108	0.0137	0.0057	0.0098	0.0099
PM10 Emissions - Front and Back Half Catch						
PM10, lb/h	34.0	34.0	34.0	18.0	34.0	46.9
PM10, lb/M8tu (LHV) (incl. duct burner fuel)	0.0185	0.0230	0.0292	0.0127	0.0210	0.0223
PM10, Ib/MBtu (HHV) (incl. duct burner fuel)	0.0173	0.0216	0.0274	0.0114	0.0197	0.0207
PM 10 with the Effects of SO2 Oxidation [includes [MHJ]2.(SO4)]	56, 14 SW(FA), \$5,900	2500-2000/00/2005/2005/2005	MARIS NO CONTRACTOR	2012/2014/05/2014/2014	(SEC.) (SEC.) SEC.) (SEC.) (SE	0.000 (0.000 (0.000)
PM10 Emissions - Front Helf Catch Only						
PM10, lb/h	17.0	17.0	17.0	9.0	17.0	22.4
PM10, tb/MBtu (LHV) (incl. duct burner fuel)	0.0092	0.0115	0.0145	0.0063	0.0105	0.0100
PM10, Ib/MBtu (HHV) (Incl. duct burner fuel)	0.0067	0.0108	0.0137	0.0057	0.0098	0.0096
PM 10 Emissions - Front and Back Half Catch						
PM10, lb/h	36.7	36.2	35.7	26.2	36,4	51.2
PM10, fb/MBtu (LHV) (incl. duct burner fuel)	0.0200	0 0245	0.0307	0.0184	0.0224	0.0243
PM10, Ib/MBtu (HHV) (incl. duct burner fuel)	0.0187	0.0230	0.0288	0.0166	0.0211	0.0226
Total Effects of BO2 Oxidation	1700000072 NAC-120000	\$6824.77 TOPOCC	<b>克利尼亚岛南部</b>	(A) できたからなからだ。	30.000mm(2.74mm)300	LANCE THREE VEGE
Total SO2 to SO3 conversion rate, %vol	44.1%	44.1%	44.1%	44.1%	44.1%	36.7
Total Amount of SO2 converted to SO3, fb/h	1.33	1.07	0.84	3,96	1.17	2.11
Maximum Stack Ammonium Sulfate [(NH4)2-(SO4)] (assuming 100% conversion from SO3), but	2.75	2.20	1.74	8.16	2.42	4.33
Maximum Stack H2SO4 (assuming 100% convension from SO3 to H2SO4), lb/h	2.04	1.64	1.29	6.06	1.80	3.21
		L		L		

#### Post Combustion Emissions Control Equipment

Selective Catalytic Reduction (SCR)	S. 7007-1400/574 (A. 6007)	20000000000000000000000000000000000000	2230X3E 3073998	\$190,000,000,000,000	2.71.11.11.11.11.74.74.74	COSTO FOR MANAGED AND
NOx Removed in SCR, %wt	81,0%	81.0%	81.0%	77.8%	81.0%	78.7%
NOx removed in SCR, Ib/h	263.5	211.8	166.9	40.9	232.2	259.7
Arramonia Sip, &/h	14.3	11.5	9.0	21 0	12.6	16.2

- The emissions estimates shown in the table above are per stack.
  The dry air composition used is 0.98% Ar, 18.00% N2 and 20.99% O2
  Standard conditions are defined as 60 F, 14.696 pala, Norm conditions are defined as 60 F, 14.696 pala, Norm conditions are defined as 0 C, 1,100 ber

- 3. Standard conditions are defined as 60 F. 14.585 pas, Norm conditions are defined as 0 C. 1,103 ber
  4. All porn values are based on CH4 cabbration gas
  5. The CTG performance is from GTP, a General Electric estimation program.
  6. The HZO increase it the SCR catalyst is negripible and not included in the analysis.
  7. The VOC/LHC ratio is assumed to be 20% for NG and 50% for disablate.
  8. Ammonium suffates created downstream of the SCR are included in the back half particulates. The assumption that 100% SO3 is convented to ammonium suffates results in "worst case" particulate emissions.
- Where manufacturer data of bith of polutant emissions were evaliable, the greater of the manufacturer's estimate and B&Vs estimate was associated where applicable.
- Duct burner emissions are included. The duct burner pollutant emissions are Black & Vestch estimates based on low NOx duct burner emissions data (provided by Forner).
- The front half catch of CT perticulate emissions is assumed to be half the amount of the front and back half catch
   As requested the SCR was designed to reduce the NOx stack emissions to 2 and 8 ppmvd@ 15%O2 when firing NG and
   Disblare, respectively.
- Displace, respectively.

  13. The emissions estimate is based on FGT pas with a maximum sulfur content of 2.0 grains/100scf.

FMPA				
Treesure Coast Energy Center Unit 1				
Black & Vestch Project 13856.0030 1x1 Emissions Estimates				
Case Number	66	67	68	69
CTG Model	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type CTG Load	Natural Gas 40%	Natural Gas 40%	Natural Gas 40%	Hatural Gas 40%
CTG Inlet Air Cooling	Of	Off	Off	Of
CTG SteenvWater Injection Ambient Temperature, F	No. 100	No 73	No 56	No 26
HRSG Duct Firing Fuel Suttur Content (grains/100 standard cubic feet)	Unfired 2.00	Unfired 2.00	Unfired 2.00	Unfired 2.00
·				
Ambient Conditions				
Ambient Temperature, F  Ambient Relative Humidity, %	100.0	73.0 81.5	59 0 60.0	25.0 100.0
Atmospheric Pressure, psie	14.990	14.690	14.690	14 690
Combustion Turbine Performance				
		GTP	GTP	GTF
CYG Performance Reference	GTP	GIP		
CTG Inlet Air Conditioning Effectiveness, % CTG Compressor Inlet Dry Bulb Temperature, F	100.0	73.0	0 59.0	26.0
CTG Compr. Inlet Relative Humidity, %	48.5	81.6	60.2	100.0
Inlet Loss, In. H2O	4.0	4.0	40	4.0
Exhaust Loss, in. H2O	5.2	5.6	5.8	5.0
CTG Load Level (percent of Base Load)	40%	40%	40%	40%
Gross CTG Output, xW	57,800	64,800	67,500_	73,400
Gross CTG Heet Rate, BrufsWh (LHV) Gross CTG Heet Rate, BrufsWh (HHV)	14,440 16,018	13,740 15,241	13,520 14,997	13,140 14,578
Gross CTG Heat Rate, BruntvVh (HHV)				
CTG Heat Input, MSturh (LHV) CTG Heat Input, MSturh (HHV)	834.6 925.8	690.4 987,6	914 0 1,013.8	964.5 1,069.9
CTG Water/Steem Injection Flow, Buth Injection Fluid/Fuel Ratio	0.0	0.0	0 0 0	0.0
CTG Exhaust Flow, Ib/h	2,092,000	2,161,000	2,197,000	2,248,000
CTG Exhaust Temperature, F	1,200	1,200	1,200	1,200
Print Combustion Turbine Fool ("Annual Company	「後人ンスを総合を	265-238894607-0	, amelina o 1969929	Variables contract
Total CTG Fuel Flow, Brh CTG Fuel Temperature, F	40,100 365	42,770 365	43,910 365	46,330 365
CTG Fuel LHV, Brutb CTG Fuel HHV, Brutb	20,816	20,816 23,091	20,816 23,091	20,816
HHV/LHV Ratio	1,1063	1.1093	1,1093	1.1093
CTG Fuel Composition (Ultimate Analysis by Weight)				
c	0.00% 73.78%	0.00% 73.76%	0.00% 73.76%	0.00% 73.78%
HZ	24.01%	24.01% 0.61%	24.01% 0.61%	24.01%
N2 O2	_1.61%	1.61%	1.61%	1,619
S	0.00857% 100.00%	0.00657% 100.00%	0 00957%	0.00857%
Fuel Sulfur Content (grains/100 standard cubic feet)	2.00	2.00	2.00	2.00
Combustion Turbine Exhaust				
学 SaCTO Exhibited Analyses (Volume Baste Wed) するかな デニット かんこのであることが明しいを明かない かまれて かってできなか	W. 996-2754-276	Carried and a superior of the		
	0.92%		<b>教育のなどの問題のなってなってが、対象的</b>	(2) (40) (80) (80) (80) (80) (80)
C02		0 93%	0 94%	0.949
	3.32% 9.51%	0 93% 3.44% 8.85%	0 94% 3 49% 7.76%	0.945 3.605
N2 O2	9.51% 73.11%	3.44% 8.85% 73.71%	0 94% 3 49% 7.76% 74 60%	0.949 3.609 7.459 74.929
O2 SO2, (effer SO2 oxidation)	9.51% 73,11% 13,14% 0.00009%	3.44% 8.85% 73.71% 13.07% 0.00009%	0 94% 3 49% 7.76% 74 60% 13.22% 0.00009%	0.945 3.605 7.452 74.925 13.065 0.000105
02	9.51% 73.11% 13.14%	3.44% 8.85% 73.71% 13.07%	0 94% 3 49% 7.76% 74 60% 13.22%	0.949 3.609 7.459 74.921 13.069 0.000109 0.000029
02 S02 (after S02 exidention) S03 (after S02 exidention) Total	9.51% 73.11% 13.14% 0.00009% 0.00002% 100.0%	3.44% 8.85% 73.71% 13.07% 0.00009% 100.0002%	0 94% 3 49% 7,78% 74 60% 13.22% 0 00009% 0 00002%	0.941 3.607 7.451 13.061 0.000101 0.00021
02 S02 (refer S02 exidation) S03 (refer S02 exidation) Total  Milecular VM, St/mol Specific Volume, p1/Vb	9.51% 73.11% 13.14% 0.00002% 0.00002% 100.0%	3.44% 8.85% 73.71% 13.07% 0.00009% 100.00% 28.31	0 94% 3 45% 7 76% 74 60% 13 22% 0 00009% 100 0%	0,941 3,607 7,452 13,069 0,00010 ⁴ 0,00021 100.0 ⁴
O2   SO2, (ethar SO2 exidation)   SO3, (ethar SO2 exidation)   Total	9.51% 73.11% 13.14% 0.00009% 0.00002% 100.0%	3.44% 6.85% 73.71% 13.07% 0.00009% 0.00002% 100.0%	0 94% 3 45% 7.76% 74 60% 13 22% 0 00009% 0 00002% 100 0% 28 44 42 03 13.38 999	0.941 3.607 7.457 74.922 13.061 0.0000024 100.061 28.44 41.94
O2 SO2, (after SO2 codation) SO3, (after SO2 codation) Total Molecular VM, Brinol Specific Volume, x7Vb Specific Volume, x6tib	9.51% 73.11% 13.14% 0.00009% 0.00002% 100.0% 28.23 42.40	3.44% 8.55% 73.71% 13.07% 0.00009% 100.0002% 100.003 28.31 42.23 13.40	0 94% 3 49% 7 76% 74 60% 13 22% 0 00009% 0 00002% 100 0% 28 44 42 03 13.34	0,941 3,607 7,451 13,069 0,00010 0,00021 100,00 28,44 41,94 13,37 1,571,353
O2 SO2 (after SO2 esidation) SO3 (after SO2 esidation) Total  Melecular VM, Brimol Spacefic Volume, ph/Vb Spacefic Volume, ph/Vb Spacefic Volume, actity Enhant Case Flow,	9 51% 73.11% 13.14% 0.00009% 100.00% 100.00% 120.22 42.40 13.44 1.478,347 468,606	3.44% 8.85% 73.71% 13.07% 0.00009% 0.00009% 100.0% 128.31 44.23 13.40 15.20,964	0 94% 3 45% 7 76% 74 60% 19 22% 0 00002% 1 00 00% 28 44 4 42 93 13.34 1,538 609	0.9419 3.600 7.401 74.921 13.080 0.00010 0.00010 100.00 28.44 41.94 13.37 1,371,385
O2 SO2, (after SO2 exidation) SO3, (after SO2 exidation) Total  Medicular VA, Brimot Spacefic Volume, n°1/10 Spacefic Volume, aftith Entheast Gas Flow, actith Entheast Gas Flow, actim	9 51% 73 11% 13 14% 0 00002% 100 0% 100 0% 28 23 42 40 13 44 1,476,347 455,008	3.44%, 0.85%, 73.71%, 0.0009%, 0.0002%, 100.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%, 120.0%	0 94% 3 45% 7.76% 74 90% 13 22% 0 00009% 0 00002% 100 0% 28 44 42 03 13.38 969 488,466	0.9419 3.600 7.401 74.921 13.080 0.00010 0.00010 100.00 28.44 41.94 13.37 1,371,385
O2 SO2, (after SO2 exidation) SO3, (after SO2 exidation) Total Malecular VM, Brind Specific Volume, ArVIb Specific Volume, ArVI Additional Proceed Margin Included in mass based NOx Emissions below NOx, pprovid (dry, 15% O2)	9 51% 73 11% 9 13 11% 0 00009% 0 00002% 100 0% 28 22 42.40 11.479,347,468,606	3.44% 6.85% 72.71% 0.00000% 0.00000% 100.00% 28.31 42.22 13.40 45.203 45.203 45.203 94.407.2888667 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.40 95.	0.94% 3.49% 7.70% 7.460% 19.22% 0.00009% 100.005 100.005 100.006 28.44 42.03 13.39,999 488,499	9,949 9,000 7,459 74,579 13,000 0,00007 0,00007 100,00 28,41,51 13,33 49,056
O2 SO2 (effer SO2 exiderion) SO3 (effer SO2 exiderion) Total  Melecular VM, Strnot Specific Volume, (h1Vb) Specific Volume, eff Vb Additional Parcinet Melanut Post Combinations Enrications Enriched Volume, eff Vb Additional Parcinet Melanut Post Combinations Enrications Delow	9 51% 73.11% 0.0002% 0.0002% 100.0% 120.0% 122.4 13.44 1.478,347 468,006	3.44% 0.85% 73.71% 13.07% 0.00002% 100.00% 28.31 42.23 13.40 42.23 42.23 43.623 40.623 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 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60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60.600 60	0.94% 3.45% 7.75% 7.465% 19.22% 0.000092% 100.0% 132.34 4.97.00 133.34 1,530.898 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 4.97.00 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O2 SO2, (effer SO2 exidation) SO3, (effer SO2 exidation) Total  Melacular VM, Brimot Specific Velume, 作がか Specific Velume, effer Enhant Cas Flow, edith Enhant Cas Flow, edith Enhant Cas Flow, edith Additional Purcurel Welthook Post Combortion Emissions Depting) (中海地域・中海地域はアントの大阪の大阪の大阪の大阪の大阪の大阪の大阪の大阪の大阪の大阪の大阪の大阪の大阪の	9 51% 73.11% 9.0002% 9.0002% 100.0% 28 29 42.40 13.44 1.478,347 468,006 67.24 (1.48) 61.00 67.40 79.10 289.7	3.44%, 6.85%, 72.71%, 13.07%, 0.00009%, 0.00009%, 100.0%, 13.00%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.50%, 13.5	0.94% 3.69% 7.76% 7.80% 19.22% 0.000092% 100.0% 128.44 42.00 1.3.35,96% 45.00 0% 45.00 0% 45.00 0% 9.00 10.00 9.20 10.00 9.20 10.00 9.20 10.00 9.20 10.00 9.20 10.00 9.20 10.00 9.20 10.00 9.20	0.944 3.007 7.455 7.427 13.061 0.000071 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.07 100.
O2 SO2, (after SO2 exidation) SO3, (after SO2 exidation) SO3, (after SO2 exidation) Total Malescutar VM, Brind Specific Volume, Art VMb Additional Procure Margin Included in mass based MOx Emissions below NOx, permit (dry, 15% O2)	9 51% 73 11% 13.14% 0.00009% 0.00009% 100.0% 42.00 13.44% 13.44% 13.44% 14.479,247 450,608	3 44%, 6.85%, 72.71%, 13.07%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%, 6.85%,	0.94% 3.40% 7.70% 7.460% 19.22% 0.00002% 0.00002% 428.44 42.00 13.33% 1.358,999 459,409 0.000 9.000	0.944 3.807 7.452 7.452 13.000 0.00007 0.00007 100.07 110.07 419.05 419.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.05 49.
O2 SO2, (after SO2 exidation) SO3, (after SO2 exidation) SO3, (after SO2 exidation) Total Malecular VM, Brind Specific Volume, APVID ADSIGNATION OF SPECIFIC VOLUME NO, permit (dry, 15% O2)	9 51% 73 11% 13.11% 0.00009% 0.00009% 100 0% 28 22 42.90 13.44 1,476,347 488,608 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00 675,243 881,00	3 44% 6 85% 72 71% 13 07% 6 00000% 6 00000% 100 05% 120 31 42 22 13 44 45,823 14 45,823 100 36 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 37 100 3	0.94% 3.45% 7.70% 7.46% 19.22% 0.00003% 0.00003% 42.44 42.03 13.34% 1.259,899 468,489 9.00 9.20 10.000 9.20 3.30 0.0008	0.944 3.807 7.407 17.407 13.007 10.0007 100.007 100.007 100.007 100.007 100.007 100.007 100.007 100.007 100.007 100.007 100.007 100.007 100.007 100.007 100.007 100.007 100.007
O2 SO2, (after SO2 exidation) SO3, (after SO2 exidation) SO3, (after SO2 exidation) Total Malescutar VM, Brind Specific Volume, ArVib Additional Purcuret Margin Included in mass based NOx Emissions below NOx, ppmvd (dry, 15% O2)	9 51% 73 11% 13.14% 0.00009% 0.00009% 100 0% 12.22 42.90 13.44% 1.476,347 469,005 610 6110 6740 779 10 289 77 0.3322 0.2313	3 44% 6 85% 72 71% 13 197% 0 00009% 0 00009% 100 05% 20 31 42 22 13 40 1,520,894 45,823 100,30 100,30 20 30 100,30 20 30 100,30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 30 20 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O2 SO2, (after SO2 exidation) SO3, (after SO2 exidation) Total  Molecular VR, Brind Specific Volume, (1795) Additional Parcent Margin included in mass based HOx Emissions below  NOx, permet (1797) HOx, permet (1797	9 51% 73 11% 9 00002% 9 00002% 100 0% 28 29 42 40 13 44 1479,347 466,606 779 10 2897 0 2292 0 2713 0 3222 0 2713 0 00002 0 00000 0 00000 0 00000 0 00000 0 00000 0 00000	3 44% 6 85% 72 71% 13 07% 0 000000% 10 00000% 10 00000% 10 00000% 10 13 30 13 40 13 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10 13 14 10	0.94% 3.49% 7.76% 7.26% 7.26% 13.27% 0.00002% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0% 100.0	200 100 100 100 100 100 100 100 100 100
GO_ (effer SO2 exidation) SO3_ (effer SO2 exidation) SO3_ (effer SO2 exidation) Total Makendar VM, Brind Specific Volume, Art VMb Additional Provent Margin included in mass based MOx Emissions below  NOx, permit (dry, 15% OZ) NOx, British CHVV) NOx, British CHVV) NOx, British CHVV) NOx, British CHVV Additional Provent Margin included in mass based CO Emissions below  Additional Provent Margin included in mass based CO Emissions below  CO, permit (dry, 15% OZ) CO, permit (dry, 15% OZ) CO, permit (dry, 15% OZ) CO, British (HVV) Additional Provent Margin included in missa based CO Emissions below  Additional Provent Margin included in missa based CO Emissions below  Additional Provent Margin included in missa based CO Emissions below  Additional Provent Margin included in missa based CO Emissions below  Additional Provent Margin included in missa based CO Emissions below  Additional Provent Margin included in missa based CO Emissions below  Additional Provent Margin included in missa 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### Additional Present Namy in Section 1995   0.075   0.075   0.075	
Total Facilitation Estimates   Feb.   For   Fo	- 6
CEN SAMES   PROPERTY   POTON	- 6
CTG   Law   Cooling	
CTG   Leaf   A Country   Leaf   Leaf   Leaf   A Country   Leaf	
CTC1 band Code	P
CTG Stans-Private Specifics	Natur
Transport   Tran	
Anchant Transporture, F Fixed Date Transporture, F Fixed Date Content (grainer 100 standard rotals hard) Fixed Date Content (grainer 100 standard rotals hard) Fixed Date Content (grainer 100 standard rotals hard)  Complication Turbrine Exhants - content (grainer 100 standard rotals hard)  Complication Turbrine Exhants - content (grainer 100 standard rotals hard)  Additional Provent Mergan rotals and Part Content (grainer 100 standard rotals hard)  Additional Provent Mergan rotals and Public Entertains Between  100	
Intelligible Control (groups) (20 standard code) (see)   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00   2.00	
Total Space Convent (grammar 100 care channels - confidence)  Compositions Turbrise Schwart - confidence  Compositions (Methods Part Commissions Entering)  Commissions (Methods	
Additional Process Manages (Included in Brit Used Emissions Delever   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%   0.0%	`
Additional Process National National Process National Services National Services National Nat	
Additional Procent Manages Included in Bits UNICE Envisions Below  UNICE, permet latery, 1996, 079  120, 200, 200, 200, 200, 200, 200, 200,	Service of the servic
UHC, permit (dry, 19% CO2)  UHC, permit (dry)  123 224 74 76  UHC, permit (dry)  123 225 76  124 225 76  UHC, permit (dry)  125 22 22 76  UHC, permit (dry)  126 22 22 76  UHC, permit (dry)  127 22 22 76  UHC, permit (dry)  128 22 76  UHC, permit (dry)  129 000000000000000000000000000000000000	
UHC, power (ent)  12.8  22.8  7.6  UHC, power (ent)  23.5  23.6  23.4  9.0  UHC, power (ent)  12.5  23.6  23.4  9.0  12.5  23.6  23.4  9.0  12.5  12.5  23.6  23.4  9.0  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5  12.5	
UHC, ported (etc.)  UHC, p	
USC, Darting and CH4 (LVM)  OD006  OD	
UHC, BATHER S. CHM (MY)  0.0009  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.00000  0.000000	
URC by Differ in CH4 (HM) 0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.00000   0.00000   0.000000   0.00000000	
CTS VOC Envisions (Without Post Companions Envisions below   Post Companions   Pos	
Actioned protection may broated in this NOC architecture between DN ON	
Additional percent margin included in Bift VCC contributors believe   0%   0%   0%   0%   0%   0%   0%   0	4 3 X 1 X 1 X 1 X 1 X 1 X 1 X 1 X 1 X 1 X
VOC. percentage of UPC   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%   20%	THE COLUMN
VCC, ported (dr), 15% CQ    4.4	
VCC, ported (dr), 15% CQ    4.4	
VOC. permit (90)	
VCC, perfect (well)	
MOC. But But as CH4 (HV)   0.0001   0.0007   0.0000     VCC, But But as CH4 (HV)   0.0005   0.0001   0.0010     VCC, Dut But as CH4 (HV)   0.0005   0.0001   0.0010     VCC, Dut But as CH4 (HV)   0.0005   0.0001   0.0010     VCC, But	
VOC. But Brus a Cliff (HIV)   0.0005   0.001   0.0018	
VOC. But Brus a Cliff (HIV)   0.0005   0.001   0.0018	
Percent margin included in PM10 amissions below   0%   0%   0%   0%   0%   0%   0%   0	
Percent margin included in PM10 amissions below   0%   0%   0%   0%   0%   0%   0%   0	4176100455807
PM10, bh/Bbx (HV)	54 ( ) 46 14 ( 94 94 ) 7 ( 95 94 )
PM10, bm/Bbx (HM)	
PM10, bridBut (HM)	
PM10_bridShu (HMY)	
PM10, 8h/HB (LHM)	
PARTO_BANDS (LHY)	
PM10_bMBbs (LHV)	
PM10 Duct Burner   Plant   Plant   Duct Burner   Plant   Plant   Duct Burner   Plant	
MR30 Duct Burner   Puet   Mittor (LHV)   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0   0.0	
Duct Burner Field	
Duct Burner Heal Floor, MBNuh (LHV)	
Duct Burner Feet Input, (#Sputh (HYV)	40/15/7.619C
Duct Burner Feet Input, (#Sputh (HYV)	
Duct Burner Fuel LITV, Bruffs   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,816   20,81	
Duet Burner Fuel Composition (UBmate Analysis by Weight)   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,09	
Duet Burner Fuel Composition (UBmate Analysis by Weight)   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,091   20,09	
Duct Burner Fuel HHV, (But/b   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091   23,091	
Ar 0.00% 0.00% 0.00% 0.00% 0.00% C 0.0	
Ar 0.00% 0.00% 0.00% 0.00% 0.00% C 0.0	
C         73.76%         73.76%         73.76%         73.76%         73.76%         73.76%         73.76%         73.76%         73.76%         24.01%         24.01%         24.01%         24.01%         24.01%         24.01%         24.01%         24.01%         24.01%         24.01%         24.01%         26.01%         26.01%         24.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01%         26.01% <td></td>	
H2	
N2	
O2         1.61%         1.61%         1.61%         1.61%         1.61%         1.61%         1.61%         1.61%         1.61%         1.61%         1.61%         1.61%         1.61%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%         1.62%	
S 0.00857% 0.00857% 0.00857% 0.00857% 10.0057% 10.0057% 10.0057% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.005% 10.	
Total   100 0% 100 0% 100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%   100 0%	0.0
Fuel Suthur Content (grainer) 100 standard cubic feet) 2,00 2,00 2,00 2,00 2,00 2,00 2,00 2,0	
Duct Burner NOx, b/MBtu (HHV)         0.080         0.080         0.080	
Duct Burner NOx, Ib/MBtu (HHV)         0.080         0.080         0.080	
Duct Burner UHC (as CH4), IN/MBtu (HMV) 0.060 0.060 0.060	
Duct Burner VCC (as CH4), BMBbs (HHV) 0.004 0.004	
Duct Burner PM10, Ib/MBtu (HHV) (front half catch only) 0.010 0.010 0.010	
Duct Burner PM10, Is/MBbu (HHV) (front and back half catch) 0.024 0.024 0.024	
Assumed SO2 oxidation rate in Duct Burner, vot% 10.0% 10.0%	
Total SQ2, fulfi from Duct Burner Fuel only (after SQ2 oxidation) 0.000 0.000	
Total SO3, (br) from Duct Burner Fiel only (effer SO2 exidation)         0.000         0.000	
DB NOx. B/h 0.00 0.00 0.00	_
DB CO, Info	
DB UHC (ss CH4), Brh 0.00 0.00 0.00 0.00	
DB VOC (as CH4), Ibh 0.00 0.00 0.00	
DB PM10, lbth (front half catch only)         0.00         0.00         0.00           DB PM10, lbth (front and beck half catch)         0.00         0.00         0.00	

FMPA				
Treasure Coast Energy Center Unit 1				
Black & Vestch Project 138859.0030 1x1 Emissions Estimates				
Case Kumber	56	67	68	69
	1			
CTG Model	PG7241	PG7241	PG7241	PG
CTG Fuel Type	Natural Gas	Natural Gas	Natural Gas	Natura
CTG Load	40%	40%	40%	
CTG Inlet Air Cooling CTG Stream/Water Injection	Off No	Off No	Off No	
Ambient Temperature, F	100	73	59	
HRSG Duct Firing	Unfired	Unfined	Unfred	
Fuel Sulfur Content (grains/100 standard cubic feet)	2.00	2.00	2.00	
Stack Emissions				
Stack Ethalist Analysis - Vokume Besig - Wag 1. 1800 - 100.1855 1955 1955 1955 1955 1955	s Esser Compressions	go . ****/c./addition	575 6607 50000000000	Walas 1888987777
Ar	0.92%	0.93%	0.94%	
COZ	3.32%	3.44%	3.49%	
H2O	9.51%	8.85%	7.76%	
N2	73.11%	73.71%	74,60%	7.
οz	13.14%	13.07%	13.22%	1:
SO2 (after SO2 oxidation)	0.000080%	0.000080%	0.000000%	0.000
SO3 (after SO2 oxidation)	0.000030%	0.000030%	0 000040%	0.000
Total	100.0%	100.0%	100.0%	
Stack Exit Temperature, F	165	162	158	
Stack Diameter, it (estimated)	18	18	18	
Stack Flow, Ib/h	2,091,996	2,160,998	2,196,998	2,247
Stack Flow, scfm	468,608	482,623	488,466	499
Stack Flow, acfm	563,097	577,347	580,740	58
Stack Exit Velocity, fl/s	37.0	38.0	38.0	
The state of the s		Mark Name of the Control of the Cont		498. <b>6M</b> 020400000
		900 P 11 11 11 11 11 11 11 11 11 11 11 11 1		CDAMES CONTROL
NOx, pprivd (dry, 15% O2)	81.0	93.0	9.0	, p. 845 ; ; ; 845 ;
NOx, pprivd (dry, 15% O2) NOx, pprivd (dry)	81.0 87.4	93.0 103.2	9.0 10.0	
NOs, pprind (dry, 15% O2) NOs, pprind (dry) NOs, pprind (ref)	81.0 87.4 79.1	93.0 103.2 94.1	9.0 10.0 9.2	
NOs, pprivid (dry) NOs, ppriviv (vest) NOs, priviv (vest) NOs, bits as NO2 (britishdes correction adder)	81.0 87.4	93.0 103.2	9.0 10.0	0
NOs, pprivid (dry. 15% OZ) NOs, pprivid (dry) NOs, pprivid (vit)	81.0 87.4 79.1 269.7	93.0 103.2 94.1 330.3	9.0 10.0 9.2 33.0	0
NOs, permet (dyr. 15% CZ) NOs, permet (dyr.) NOs, permet (ew) NOs, bith as NO2 (includes consistion adder) NOs, bith as NO2 (includes consistion adder) NOs, bith Bith (LHV) as NO2 (find, duct burner hae) NOs, bithBith (HHV) as NO2 (find, duct burner hae)	81.0 87.4 79.1 269.7 0.3232 0.2913	93.0 103.2 94.1 330.3 0.3710 0.3345	9.0 10.0 9.2 33.0 0.0981 0.0328	0
NOs, permet (day, 15% OZ)  NOs, permet (day)  NOs, permet (twit)  NOs, bith as NOZ (includes consistion adder)  NOs, bith as NOZ (includes consistion adder)  NOs, bith bith (LHV) as NOZ (incl. duct burner has)  NOs, bith bith (LHV) as NOZ (incl. duct burner has)  Stack NOs, Emissions with the Effects of Belieches Catalytic Reduction (SCR) \$7.7007.	81.0 87.4 79.1 269.7 0.3232 0.2913	93.0 103.2 94.1 330.3 0.3710 0.3345	9.0 10.0 9.2 33.0 0.0961 0.0326	
NOL, permed (day, 15% OZ).  NOL, permer (day).  NOL, permer (law).  NOL, permer (law).  NOL, pin he NOZ (includes correction addler).  Stack (NOX Emissions with) the Effects of Besingthin Capitalytic Reduction (BCR) 32 7007 ADMINISTRATION NOX, permed (day, 15% OZ).	81.0 87.4 79.1 299.7 0.3232 0.2913	93.0 103.2 94.1 330.3 0.3710 0.3345	9.0 10.0 9.2 33.0 0.0361 0.0326	0
NOs., permet (dry. 15% OZ) NOs. permet (dry.) NOs. permet (dry.) NOs. pitch set NOZ (finchedes correction adder) NOs. bitch set NOZ (finchedes correction adder) NOs. bitch set NOZ (finch dust burner har) NOs. bitch set NOZ (finch dust burner har) Stack NOs. permet (dry.) 15% OZ)	81.0 87.4 79.1 269.7 0.3232 0.2913	93.0 103.2 94.1 330.3 0.3710 0.3345	9.0 10.0 9.2 33.0 0.0361 0.0328	0
NOL, permed (dry. 15% OZ) NOL, permed (dry. 15% OZ) NOL, permed (dry. 15% OZ) NOL permed (dry. 15% OZ)	81.0 87.4 79.1 259.7 0.3232 0.2913	93.0 100.2 94.1 390.3 0.3710 0.3345	9.0 1000 9.2 33.0 0.0381 0.0326 2.0 2.2 2.2	0
NOL, permet (dy.) 15% OZ)  NOL permet (dy.)  NOL permet (text)  NOL bit is NOZ (includes conscition adder)  NOL bit is NOZ (includes NOZ (incl. duct burner bas)  NOL bit is NOZ (incl.)  Stack NOL Emissions with the Effects of Beliecitys Calabytic Reduction (SCR) of PAGE ADDERSEL ATTRIBUTE  NOL permet (dw.)  NOL permet (dw.)  NOL bit is NOZ (includes NOX margin popiled to CTG)	810. 874. 79.1. 269.7 0.3232 0.2913 2.0 2.2 2.2 2.0 6.7	93.0 193.2 94.1 330.3 0.3710 0.3345 2.0 2.2 2.0 7.1	9.0 10.0 9.2 33.0 0.0081 0.0328 2.0 2.0 2.2 2.1	0 0
NOs, permed (dry. 15% OZ)  NOs, permed (dry.)  NOs, permed (two)  NOs, bith as NOZ (declades correction adder)  NOs, bith as NOZ (declades correction adder)  NOs, bith Bith (LHV) as NOZ (field, duct burner hash)  NOs, bithBith (LHV) as NOZ (field, duct burner hash)  Stack (NOX Emissions wifth the Effects of Beliechtes Castalytic Reduction (SCR)   NOS, permed (dry.) 15% OZ)  NOS, permed (dry.)  NOS, bith as NOZ (fineldes NOX margin applied to CTG)  NOS, bith as NOZ (fineldes NOX margin applied to CTG)  NOS, bith as NOZ (fineldes NOX margin applied to CTG)	810, 874 4 78-1 289,7 0.3272 0.2913 3 3 3 3 3 2,0 2,2 2,0 2,0 2,0 2,0 3 3 4 7 8 1 8 1 8 1 8 1 8 1 8 1 8 1 8 1 8 1 8	93.0 193.2 94.1 390.3 0.3710 0.3345 2.0 2.0 2.2 2.0 7.1 0.0000	9.0 100 9.2 33.0 0.0981 0.0028 2.0 2.0 2.2 2.1 7.3 0.0060	0 0
NOs. permet (dry. 15% CZ)  NOs. permet (dry. 15% CZ)  NOS. permet (text)  NOS. bith as NO2 (includes conscision adder)  NOS. bith as NO2 (includes conscision adder)  NOS. bith as NO2 (first duct burner bas)  NOS. bith as NO2 (first duct burner bas)  NOS. bith as NO2 (first duct burner bas)  Stack NOs. Emissions with the Effects of Besicoting Calabytic Reduction (SCR) of PNOS Administration (NOS, ported (dry. 15% CZ)  NOS. ported (dry.)  NOS. permet (dry.)  NOS. permet (dry.)  NOS. byth as NO2 (includes NOX mannin popied to CTG)	810. 874. 79.1. 269.7 0.3232 0.2913 2.0 2.2 2.2 2.0 6.7	93.0 193.2 94.1 330.3 0.3710 0.3345 2.0 2.2 2.0 7.1	9.0 10.0 9.2 33.0 0.0081 0.0328 2.0 2.0 2.2 2.1	0 0
NOL, permet (dry. 15% OZ).  NOL permet (dry.)  NOL permet (ever)  NOL permet (ever)  NOL permet (ever)  NOL pitch is NOZ (includes correction addre)  NOL pitch is NOZ (includes correction addre)  NOL pitch is NOZ (finct, duct burner har)  NOL ported (dry. 15% OZ)  NOL permet (dry. 15% OZ)  NOL permet (dry. 15% OZ)  NOL permet (ever)	810, 874 4 78-1 289,7 0.3272 0.2913 3 3 3 3 3 2,0 2,2 2,0 2,0 2,0 2,0 3 3 4 7 8 1 8 1 8 1 8 1 8 1 8 1 8 1 8 1 8 1 8	93.0 193.2 94.1 390.3 0.3710 0.3345 2.0 2.0 2.2 2.0 7.1 0.0000	9.0 1000 9.2 33.0 0.0081 0.0082 2.0 2.2 2.1 7.3 0.0080 0.0072	0 0
NOz, permed (dry. 15% CZ)  NOz, permed (dry.)  SERVICE (First of the STOCK)  NOZ, permed (dry.)  SERVICE (First of the STOCK)  NOZ, permed (dry.)  SERVICE (First of the STOCK)	810 874 79.1 299.7 0.3272 0.2913 3 30895 2.0072 2.0 2.7 0.0072 0.0072	20.0 100.12 94.1 350.3 0.3710 0.3345 20.2 2.2 2.2 2.1 1.1 0.0000 0.0072	9.0 19.0 9.2 33.0 0.00081 0.00082 2.0 2.2 2.1 7.3 0.0000 0.00072	0 0 0
NOL, permet (dry. 15% CZ) NOL, permet (vet) NOL, permet (vet) NOL, permet (vet) NOL, bit his NOZ (includes consistion adder) NOL bit his NOZ (includes consistion adder) NOL bit his NOZ (includes NOZ (incl. duct burner has)  Stack NOX Emissions with the Effects of Belesthy's Castalytin Reduction (SCR) of Price Address of State (NOX permet (dry. 15% CZ) NOX, permet (dry. 15% CZ) NOX, permet (larty) NOX bit his NOZ (includes NOX margin populed to CTG) NOX, bit his NOZ (includes NOX margin populed to CTG) NOX bit his NOZ (incl. duct burner has) NOX bit his permet (dry. 15% CZ) SCR NNO3 sign, permet (dry. 15% CZ) SCR NNO3 sign, permet (dry. 15% CZ)	810, 874, 79.1 299.7 0.3232 0.2913 2.0 2.2 2.0 0.0077 0.00090 10.0007	930 1902 94.1 380.3 0.3710 0.3345 2.2 2.0 7.1.1 0.0000 0.0007 190.1	90 100 92 330 0.008 0.008 0.0028 2.0 2.1 7.3 0.0090 0.0077 100 135	0 0 0
NOL, permet (day, 15% C2)  NOL, permet (ear)  NOL, permet (ear)  NOL, permet (ear)  NOL, bit is NOZ (includes correction addler)  NOL, bit is NOZ (includes correction addler)  NOL bit is NOZ (includes correction addler)  NOL bit is NOZ (includes NOZ (incl. duct burner hash)  NOL permet (day, 15% C2)  NOL, permet (day, 15% C2)  NOL, permet (day)  NOL, permet (and)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL bit is NOZ (includes NOX margin applied to CTG)  NOL bit is NOZ (includes NOX margin applied to CTG)  NOL bit is NOZ (includes NOX margin applied to CTG)  NOL bit is NOZ (includes NOX margin applied to CTG)  NOL bit is NOZ (includes NOX margin applied to CTG)  NOL bit is NOZ (includes NOX margin applied to CTG)  NOL bit is NOZ (includes NOX margin applied to CTG)  NOL bit is NOZ (includes NOX margin applied to CTG)  NOZ (bit includes NOX margin applied to CTG)	81.0 87.4 79.1 299.7 0.3272 0.2913 3 000005 2.2 2.0 6.7 0.00072 10.0 12.3	20.0 100.12 94.1 380.3 0.3710 0.3345 123.2 2.0 2.1 2.1 1.0 0.0000 0.0072	9.0 190, 9.3 330, 0.0081 0.0028 2.0 2.2 2.1 7.3 0.00090 0.0072	0 0 0
NOL, permet (dry. 15% CZ) NOL, permet (vet) NOL, permet (vet) NOL, permet (vet) NOL, bit has NOZ (includes correction adder) NOL, bit has NOZ (includes correction adder) NOL, bit has NOZ (includes correction adder) NOL, bit has NOZ (incl. duct burner has)  ### Stack NOL (includes NOZ (incl. duct burner has)  ### Stack NOL (includes NOZ (incl. duct burner has) NOL, permet (dry. 15% CZ) NOL, bit has NOZ (incl. duct burner has) NOL bit has NOZ (incl. duct burner has) NOL bit has NOZ (incl. duct burner has) NOL bit has bit has NOZ (incl. duct burner has) NOL permet (dry. 15% CZ) COL permet (dry. 15% CZ)	810, 874 / 79.1 299.7 0.3232 0.2913 2.0 2.2 2.0 6.7 0.0009 0.0077 110.0	20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (20.0 (	90 100 92 330 0008 0008 20 22 21 73 00090 00077	0 0 0
NOL, permed (dry. 15% CZ)  NOL, permed (dry.)  NOL, permed (try.)  NOL, permed (try.)  NOL, bit has NOZ (mich.dea correction addler)  NOL, bit has NOZ (mich.dea correction addler)  NOL, bit has NOZ (mich.dea borner has)  NOL, permed (dry.) as NOZ (mich.deat borner has)  NOL, permed (dry.) 15% CZ)  NOL, permed (dry.) 15% CZ)  NOL, permed (dry.)  SCR NHOL also, permed (dry.) 15% CZ)  SCR NHOL also, permed (dry.) 15% CZ)  SCR NHOL also, bith  Stands CD Emisphorus Processor (dry.)	810 874 791 299.7 0.3272 0.2913 5 20845	20.0 (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.2) (10.	9.0 190. 9.2 330. 0.0081 0.0028 2.0 2.1 7.3 0.0009 0.0072	0 0 0 0 0 0 0 0 0 0
NOS, permet (dry. 15% CZ) NOS, permet (vex) NOS, permet (vex) NOS, permet (vex) NOS, bit is in NOZ (includes correction adder) NOS, bit is in NOZ (includes correction adder) NOS, bit is in NOZ (includes correction adder) NOS, bit is in NOZ (incl. duct burnet field)  Stack MOS (Brissations with the Effects of Belesthy's Calabytic Reduction (SCR) or Policy Correction (NOZ, permet (dry. 15% CZ) NOS, bit is NOZ (incl. dash NOX margin popied to CTG) NOS, bit is NOZ (incl. dash NOX margin popied to CTG) NOS, bit is NOZ (incl. dash NOX margin popied to CTG) NOS, bit is NOZ (incl. dash Durnet field) NOS, permet (dry. 15% CZ) CO, permet (dry. 15% CZ)	810, 874 / 79.1 299.7 0.2272 0.2213 2.0 0.279 0.0079 0.0077 10.0 12.3 25.6 27.8 25.2 5.2 5.2 5.2 5.2 5.2 5.2 5.2 5.2 5.	200 10022 94.1 350.3 0.3710 0.3345 202 2.2 2.0 7.1 0.0000 0.0072 10.0 12.1	9.0 10.0 9.2 33.0 9.0 9.3 33.0 9.0 9.0 9.0 9.0 9.0 9.0 9.0 9.0 9.0 9	0 0 0
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NOs., permet (ety.) 15% CD;  NOs. permet (ety.)  NOs. permet (ety.)  NOs. bit his NOZ (includes correction side(e))  NOs. bit his NOZ (includes correction side(e))  NOs. bit his NOZ (incl.) duct burner hash  NOs. bit his NOZ (incl.) duct burner hash  NOs. permet (ety.) 15% CD;  NOs. permet (ety.) 15% CD;  NOs. permet (ety.) 15% CD;  NOs. permet (ety.)  NOS. bit his NOZ (incl. duct burner hash)  NOS. bit his NOZ (incl.) duct burner hash)  NOS. bit his NOZ (incl.) duct burner hash)  NOS. bit his NOZ (incl.) duct burner hash)  SCR NNS also, bit his NOZ (incl. duct burner hash)  SCR NNS also, bit his NOZ (incl.) duct burner hash)  SCR NNS also, bit his NOZ (incl.) duct burner hash)  SCR NNS also, bit his NOZ (incl.) duct burner hash)  SCR NNS also, bit his NOZ (incl.) duct burner hash  SCR NNS also, bit his NOZ (incl.) duct burner hash  SCR NNS also, bit his NOZ (incl.) duct burner hash  SCR NNS also, bit his NNS (incl.) duct burner hash  SCR NNS also, bit his NNS (incl.) duct burner hash  SCR NNS also, bit his NNS (incl.) duct burner hash  CO (bit NNS (INV) (bit duct burner hash)	81.0 87.4 79.1 299.7 0.3232 0.2913 5 000005	\$0.0 100.2 94.1 380.3 0.3710 0.3345 2.2 2.2 2.2 2.7 7.1 0.0000 0.0077 10.0 13.1	80 190 93 330 00991 00995 20 22 21 73 30 00990 100 110 110 100 110 100 100 100	0 0 0
NOL, permet (day, 15% CZ).  NOL, permet (wet)  NOL, permet (wet)  NOL, Britis & NOZ (Includes correction adder)  NOL, Britis & NOZ (Includes correction adder)  NOL, Britis & NOZ (Includes correction adder)  NOL, Britis & NOZ (Includes CD)  Robert (NOL Emissions wift) (the Effects of Beliesflyte Catalytis Reduction (SCR) of Price (15% CZ)  NOL, permet (day, 15% CZ)  NOL, permet (day)  NOL, britis & NOZ (Includes NOL margin applied to CTG)  NOL, britis & NOZ (Includes NOL margin applied to CTG)  NOL, britis & NOZ (Includes NOL margin applied to CTG)  NOL, britis (Lifty) as NOZ (Incl. duct burner fuel)  SCR NH3 also, permet (day, 15% CZ)  SCR NH3 also, permet (day, 15% CZ)  SCR NH3 also, britis (day)  SLack CO Emissions (Margin and Catalytis (Margin applied (Margin and Margin applied (Margin and Margin applied (Margin and Margin and Margin applied (Margin and Margin and	81.0 87.4 79.1 299.7 0.3272 0.2913 5 DANSAS - LEAVELDING 2.0 0.7 0.0000 0.0007 110.0 12.3 2.5 2.0 2.7 0.0000 0.0007 12.3 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5	\$0.0 100.2 94.1 300.3 0.3710 0.3345 2.2 2.2 2.7 7.1 0.0000 0.0072 100 121 242 249 9 9 9 100 100 100 100 100 100	8.0 190. 9.3 330. 0.0091 2.0 2.2 2.1 7.3 0.0090 0.0077 10.0 13.5 5.5 18.0 0.0178 19.0 0.0178 19.0 0.0178 19.0 0.0178	0 0 0 0
NOL, permet (day, 15% C2).  NOL, permet (rew)  NOL, permet (rew)  NOL, permet (rew)  NOL, bit is NOZ (includes correction addler)  NOL, bit is NOZ (includes correction addler)  NOL bit is NOZ (includes Correction addler)  NOL bit is NOZ (includes Correction addler)  NOL permet (day, 15% C2)  NOL, permet (day, 15% C2)  NOL, permet (day, 15% C2)  NOL, permet (day)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL, bit is NOZ (includes NOX margin applied to CTG)  NOL, bit is NOZ (includes NOX margin applied to CTG)  CO, permet (day, 15% C2)  SCR NOJ also, bit  Stack CO Emissions is NOZ (incl duct burner Nai)  Stack CO Emissions is NOZ (includes NOX margin applied to CTG and margin)  CO, permet (day), 15% C2)  CO, permet (lay), 15% C2)  Stack SCO Emissions, after SCO Calebation is NOX (includes NOX margin applied to CTG and margin)  CO, bit NoX (Int) (incl. duct burner Nai)  Stack SCO Emissions, after SCO Calebation is NOX (includes NOX calebation is NOX	81.0 87.4 79.1 299.7 0.3272 0.2913 3 30888 2.2 2.0 6.7 0.0072 10.0 12.3 22.8 23.0 24.8 27.8 27.8 27.8 27.8 27.8 27.8 27.8 27	20.0 10012 94.1 380.3 0.3710 0.3345 2.2 2.2 2.2 2.2 2.2 2.1 1.1 0.0000 0.0072 10.0 11.1 2.2 2.9 2.9 2.9 0.0072 0.0072 0.0072 0.0073 0.0073 0.0073 0.0073 0.0073 0.0073 0.0073 0.0073 0.0073 0.0073 0.0073 0.0073 0.0073 0.0073 0.0073 0.0073 0.0073	9.0 190.0 9.2 330.0 0.00091 0.00009 2.2 2.1 7.3 3.0 0.0000 0.00072 110.0 115 5 6.1 9.0 6.3 18.0 0.00172 0.0176 0.0777 0.0778	0 0 0 0
NOs., permet (dry. 15% CZ)  NOs., permet (vert)  NOs., bit his NOZ (includes correction adder)  NOs., bit his NOZ (includes NOZ (incl. duct burner hash)  Reack, NOX, Emissions wrift) (the Effects of Beliesthyle Castalytis, Reduction (SCR) (27 PM ANDERS (NOX, permet (dry. 15% CZ)  NOS., permet (dry. 15% CZ)  NOS., permet (dry.)  NOS., bit his NOZ (incl. duct burner hash)  NOS., bit his NOZ (incl. duct burner hash)  SCR NH3 also, permet (dry. 15% CZ)  SCR NH3 also, permet (dry. 15% CZ)  SCR NH3 also, bit h  Stack CO Emissions (27 PM CZ)  CO, permet (dry.) 15% CZ)  Sch (MSS) (MY) (incl. duct burner hash)  Stack SCZ Emissions, affine SCZ (oxidation in 27 PM Assumed SCZ oxidation rate in SCR, vorth.  Assumed SCZ oxidation rate in SCR, vorth.	81.0 87.4 79.1 299.7 0.3272 0.2913 5 DANSAS - LEAVELDING 2.0 0.7 0.0000 0.0007 110.0 12.3 2.5 2.0 12.3 2.0 0.7 10.0 12.3 2.0 0.0000 0.0007 10.0 12.3 2.0 0.0 12.3 2.0 0.0 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.000000	\$0.0 100.2 94.1 300.3 0.3710 0.3345 2.2 2.2 2.7 7.1 0.0000 0.0072 100 130 130 130 140 150 150 150 150 150 150 150 15	80 190 190 2330 000051 200 22 21 7.3 0.00000 0.0077 100 101 101 101 101 101 101 101 101	0 0 0
NOL, permet (day, 15% CZ).  NOL, permet (rest)  NOL, permet (rest)  NOL, permet (rest)  NOL, bit is NOZ (includes correction adder)  NOL, permet (day, 15% CZ)  NOL, permet (day, 15% CZ)  NOL, permet (day)  SCR NH3 day, permet (day, 15% CZ)  SCR NH3 day, bit  Stack CO Emispations (day, 15% CZ)  CO, permet (day)  CO, permet (day)  CO, permet (day)  SCR NH3 day, bit  Stack CO Emispations (day)  SCR NH3 day, bit (day)  CO, permet (day)  SCR NH3 day, bit (day)	81.0 87.4 79.1 299.7 0.3272 0.2913 5 000000 0.0072 10.0 12.3 2.0 9.7 9.00000 0.0072 2.1 10.0 12.3 2.2 2.3 9.7 9.00000 0.0072 10.0 12.3 2.5 9.00000 0.00000 10.00000 10.00000 10.00000 10.0000000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.0000000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.000000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.000000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.000000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.000000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.000000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.000000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.000000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.000000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.000000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.0000000 10.00000 10.00000 10.00000 10.00000 10.00000 10.00000 10.0000000 10.0000000 10.00000000	20.0 100.12 94.1 380.3 0.3710 0.3345 120.2 2.0 2.1 2.0 2.1 1.1 0.0000 0.0072 13.1 10.0 13.1 10.0 13.1 10.0 13.1 10.0 10.0	9.0 190. 9.2 330. 0.0081 0.00081 2.0 2.2 2.1 7.3 3.0 0.0009 0.0072 110.0 115 5 18.0 0.0172 0.0172 0.0172 0.0172 0.0172 0.0072 0.0073	0 0 0
NOD, permed (day, 15% CZ)  NOD, permed twel)  NOD, bits in 80/2 (includes correction adder)  NOD, bits in 80/2 (includes CO and burner hash)  Stack NOD, permed (day, 15% CZ)  NOD, permed (day, 15% CZ)  NOD, permed (day)  NOD, bits in 80/2 (includes NOD margin applied to CTG)  NOD, bits in 80/2 (includes NOD margin applied to CTG)  NOD, bits in 80/2 (includes NOD margin applied to CTG)  NOD, bits in 80/2 (includes NOD margin applied to CTG)  NOD, bits in 80/2 (includes NOD margin applied to CTG)  SCR NHS also, permed (day, 15% CZ)  SCR NHS also, bits  Stack CO Emissions in 80/2 (includes NOD margin applied to CTG and margin)  CO, permed (day)  CO, permed (day)  CO, permed (day)  Stack SCO Emissions in 80/2 (includes CO correction as applied to CTG and margin)  CO, bits (RND) (incl. duct burner hash)  Stack SCO Emissions, affer SCO Culadion in 9/4 (incl. according to SCO, permed (day)  SLOS Emissions, affer SCO Culadion in 8/4 (incl. according to SCO, permed (day), 15% CZ)  SCO, permed (day), 15% CZ)  SCO, permed (day), 15% CZ)	81.0 87.4 79.1 299.7 0.3272 0.2913 5 DANSAS - LEAVELDING 2.0 0.7 0.0000 0.0007 110.0 12.3 2.5 2.0 12.3 2.0 0.7 10.0 12.3 2.0 0.0000 0.0007 10.0 12.3 2.0 0.0 12.3 2.0 0.0 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.000000	\$0.0 100.2 94.1 300.3 0.3710 0.3345 2.2 2.2 2.7 7.1 0.0000 0.0072 100 130 130 130 140 150 150 150 150 150 150 150 15	80 190 190 2330 000051 200 22 21 7.3 0.00000 0.0077 100 101 101 101 101 101 101 101 101	0 0 0 0 0 0 0 0 0 0

1x1 Emissions Estimates Case Number	56	67	66	69
CTG Model	PG7241	PG7241	PG7241	PG7241
CTG Fuel Type	Natural Gas	Natural Gas	Natural Gas	Natural Gas
CTG Load CTG (plot Air Cooling	40% Off	40% Off	40% Off	40% Of
CTG Steam/Water Injection	l No	Off No	Off No	No.
CTG Stepmyyater reaction Ambient Temperature, F	100	73	MO 59	76
HRSG Duct Fring	Unfred	Unfired	Unfired	Unfired
Fuel Sulfur Content (grains/100 standard cubic feet)	2 00	2.00	2.00	2.00
Stack Emissions - continued				
Stands UHC Emissions (\$1500) \$250 (\$20 August 150 Augus	*2.78***********************************	4 : Walley 1999	PARTER NAME OF	######################################
UHC, ppmvd (dry, 15% OZ)	22.0	20.5	6.8	6.6
UHC, ppmvd	23.8	72.8	7.6	7.6
UHC, ppmvw	21.5	20.8	7.0	7.0
UHC, lb/h as CH4 (includes correction adder)	25.6	25.4	90	9.0
UHC, Ib/MBtu (LHV) (Incl. duct burner fuel)	0.0306	0.0285	8900.0	0.0093
UHC, Ib/MBtu (HHV) (incl. duct burner fuel)	0 0276	0.0257	0.0069	0.0084
Stack VCC Emiliations which a contract of a secretary of the contract of the c	NEAR THE SECONDARIA	\$~4. save#66866657.14	AR DWINGSONS C	9685 + 875 256 65 5 5
VOC, pprivd (dry, 15% O2)	44	4.1	1.4	1.3
VOC, pprivid (dry)  VOC, pprivid (dry)	4.0	4.1	1.5	1.5
VOC, ppmwa (wst)	43	4.2	1.4	1.4
VOC, lb/h as CH4 (includes correction adder)	5.1	5.1	1.5	1.8
VOC, Ib/MBtu (LHV) (incl. duct burner fuel)	0.0061	0.0057	0,0020	0.0019
VOC, Ib/MBtu (HHV) (incl. duct burner fuel)	0.0055	0.0051	0.0018	0.0017
Politio without the Stacts of SDZ colleges	STONESSON SANCES	The Section Section 2	Y 2007 (1000) (1000)	JA BLOOM GORNATA LA
PM10 Emissions - Front Helf Catch Only PM10, 65/h	9.0	9.0	9.0	9.0
PM10, Is/MBtu (LHV) (incl. duct burner fuel)	0.0108	0.0101	0.0098	0,0093
PM10, Ib/MBtu (HHV) (incl. duct butter fuel)	0.0097	0.0091	0.0089	0.0084
PM10 Emissions - Front and Back Half Catch				
PM10, 8/h	18.0	18.0	18.0	18.0
PM10, ts/MBtu (LHV) (Incl. duct burner fuel)	0.0216	0.0202	0.0197	0.0187
PN(10, Ib/MBtu (HHV) (incl. duct burner fuel)	0.0194	0.0182	0.0178	0.0168
PRIO with the Effects of BOZ Oxidation (Includes (NH432-(BOA))	A-98 (A 80) (A 80)	4,0700,400000-0000000	(67) 5/2 (87) 6/2/18	1875-1777-1780-00-00-00-00-00-00-00-00-00-00-00-00-0
PM10 Emissions - Front Half Catch Only PM10, Ibh	90	90	9.0	9.0
PM10, Ib/M8tu (LHV) (incl. duct burner fuel)	0.0108	0.0101	0.0098	0.0093
PM10, Ib/MBtu (HHV) (incl. duct burner fuel)	0.0097	0.0091	0.0089	0.0084
PRITO Emissions - Front and Back Half Catch				
PM10, lb/h	21.3	21.5	21.6	21.8
PM10, Is/MBtu (LHV) (incl. duct burner fuel)	0.0255 0.0230	0.0241	0.0236	0.0726
PM10, Ib/MBtu (NHV) (incl. duct burner fuel)  Total Effects of 802 Caldetion	Physical Section	S WITHOUT ASSESSED THAT	0.0213	0.0204 627770669606032×473.76.60
Total Energy of 602 Capositor)	30.2%	30.2%	30.2%	30 2%
Total SO2 to SO3 conversion rate, 14vol Total Amount of SO2 converted to SO3, Ib/h	1,59	1.69	1.74	1.83
Maximum Stack Ammonium Sulfate ((NH4)2-(SO4)) (essuming 100% conversion from SO3), fb/h	3.28	3 49	3.59	3.78
Maximum Stack H2SO4 (assuming 100% conversion from SO3 to H2SO4), lb/h	2,43	2.59	2.66	2 81
Machine dated in 250-y (asserting) from commission many occordenated in 1250-y pain		2.39		
Post Combustion Emissions Control Equipment				
Selective Catalytic Reduction (SCR) (266) 2 . ARTIST (286) 200 (486) 4	Jan C 88 100 100 100 100	LIVE STATE OFF	CMARKS WE VIKE	1993 6 5 XXX 5 . 1 8 1 15
NOx Removed in SCR. Net	97.5%	97.8%	77.8%	77.8%
NOx removed in SCR, buth	263.1	323.2	25.7	27.2
Armenia Sip, Ibh	12.3	13.1	13.5	14.2
	I			
The emissions estimates shown in the table above are per stack.				
2. The dry sir composition used is 0.98% Az. 78.03% N2 and 20.99%C2 3. Standard conditions are defined as 60 F. 14.696 psis. Norm conditions are defined as 0 C. 1.103 ber				
4. All ppm values are based on CH4 calibration cas.				
5. The CTG performance is from GTP, a General Electric estimation program. The CO, UHC & VOC emissions at 40				
percent load were adjusted based on engineering judgement.				
6. The H2O increase in the SCR catalval is negligible and not included in the anelysis.				
7, The VOC/UHC ratio is assumed to be 20% for NG and 50% for distillate.				
<ol> <li>Ammorism suffices created downstream of the SCR are included in the back half particulates. The assumption that 100% SO3 is converted to ammonium suffices results in "worst case" particulate emissions.</li> </ol>				
<ol> <li>Where manufacturer date of fulf of politiant emissions were evaluable, the greater of the manufacturer's estimate and B&amp;V's estimate was used in the summary table, i.e. the B&amp;V estimates were educated, were applicable.</li> <li>Duct burner emissions are included. The duct burner politiant emissions are Black &amp; Vestch estimates based on later.</li> </ol>				
BMVs estimate was used in the summare table, i.e. the BMV estimates were addicated, were applicable.  10. Duct burner emissions are included The duct burner pollutant enrissions are Black & Vestch estimates besed on low.  10. duct burner emissions des included the former).				
B&Vs estimate was used in the summary table, i.e. the B&V estimates were adducted, were applicable.  10. Duck burne emissions are included. The duct turner pollutant emissions are Black & Vestch estimates besed on low BKOs duct burner emissions date forwinded by Forney.  11. The front half catch of CT particulate emissions a assumed to be half the emiount of the front and back half catch.				
BMVs estimate was used in the summare table, i.e. the BMV estimates were addicated, were applicable.  10. Duct burner emissions are included The duct burner pollutant enrissions are Black & Vestch estimates besed on low.  10. duct burner emissions des included the former).				

# FMPA - Treasure Coast Energy Center (Unit 1)

Determination of Representative Emission and Stack Parameters at 100% Load

				Distillate Oi	ı								Natural Gas			
bient Temperature - 100	•F								Ambient Temperature - 100 °	F						
Case Number:	2	8	64	65	Worst Case Parsmet	ers			Case Number:	1	7	45	63	Worst Case Peramet	ers	
Evap. Cooler	X	X							Evap. Cooler	Х	×					
Duct Burner Firing	×			X					Duct Burner Firing	×		X				
Exit Temp (*F)	250	266	263	249	Exit Temp	249.0 °F	393.71 K		Exit Temp (°F)	168	184	166	181	Exit Temp	168.0 °F	347.59 K
Exit Velocity (ft/s)	71	72	69	68	Exit Velocity	68.0 ft/s	20.7264 m	1/5	Exit Velocity (ft/s)	60	61	58	59	Exit Velocity	58.0 ft/s	17.6764 m/
Emissions (lb/h)					Emissions				Emissions (lb/h)					Emissions		
NOX	73.2	57.1	54.6	70.2	NOX	73.2 lb/h	9.2230 g	/s	NOX	18.1	12.2	15.6	11,7	NOX	16.1 lb/h	2.0288 g/s
co	82.3	60.1	58.2	79.8	co	82.3 lb/h	10.3696 g	/5	co	49.2	27.0	48.6	26.1	co	49.2 lb/h	6.1991 g/s
PM/PM10	49.8	35.7	36.4	51.2	PM/PM10	51.2 lb/h	6.4511 g	/\$	PM/PM10	38.0	23.8	38.0	26.2	PM/PM10	38.0 lb/h	4.7879 g/s
SO2	5.9	2.8	2.7	5.7	SO2	5.9 lb/h	0.7446 g	/s	SO2	12.6	9.4	12.2	9.0	SO2	12.8 lb/h	1.5816 g/s
bient Temperature - 73 °	F								Ambient Temperature - 73 °F							
One March		40			Wares Garage				Cose Number	5	11			Worst Case Paramet	978	
Case Number:	6	12			Woret Case Paramet	ers			Case Number:	X	11 X			THUISI CASE FAIRMEN		
Evap. Cooler	X	X							Evap. Cooler	×	^					
Duct Burner Firing	×								Duct Burner Fining							
Exit Temp (°F)	251	265			Exit Temp	251.0 °F	394.62 K		Exit Temp (°F)	168	182			Exit Temp	166.0 °F	348.71 K
Exit Velocity (ft/s)	74	75			Exit Velocity	74.0 ft/s	22.5552 m		Exit Velocity (ft/s)	63	63			Exit Velocity	63.0 ft/s	19.2024 m/
Emissions (lb/h)	,,				Emissions	14.0 100			Emissions (lb/h)					Emissions		
NOX	76.0	60.0			NOX	76.0 lb/h	9.5758 g	/=	NOX	16.5	12.7			NOX	16.5 lb/h	2.0790 g/s
					CO	86.2 lb/h	10.8610 g		co	50.1	28.3			co	50.1 lb/h	6.3125 g/s
CO	88.2	64.0			PM/PM10	49.9 lb/h	6.2873 g		PM/PM10	38.0	24.1			PM/PM10	38.0 lb/h	4.7879 g/s
PM/PM10 SO2	49.9 6.0	35.8 2.9			SO2	6.0 lb/h	0.2673 g 0.7616 g		SO2	12.9	9.8			SO2	12.9 lb/h	1.6246 g/s
nbient Tamperature - 59 *	F								Ambient Temperature - 59 °F							
Case Number:	57	56	59	60	Worat Case Parsmet	ars			Case Number:	50	51	52	53	Worst Case Paramet	era	
Evap. Cooler		X		×					Evap. Cooler	X	×					
<b>Duct Burner Firing</b>	X	×							Duct Burner Fining	Х		×				
Exit Temp (°F)	251	251	262	263	Exit Temp	251.0 °F	394.82 K		Exit Temp (°F)	167	180	166	180	Exit Temp	166.0 °F	347.59 K
Exit Velocity (ft/s)	76	77	77	78	Exit Velocity	76.0 ft/s	23.1648 л		Exit Velocity (ft/s)	65	66	64	65	Exit Velocity	64.0 ft/s	19.5072 m/
Emissions (lb/h)	70	"	"	70	Emissions	10.0 .45	20,70 10 11		Emissions (lb/h)					Emissions		
NOX	77.3	76.0	61.4	62.0	NOX	78.0 lb/h	9.8278 g	/s	NOX	16.9	13.1	16.7	12.9	NOX	16.9 lb/h	2.1294 g/s
CO	68.0	86.7	65.9	66.6	CO	88.7 lb/h	11.1760 g		co	51.4	30.0	51.0	29.4	CO	51.4 lb/h	6.4763 g/s
PM/PM10	51.9	52.0	36.7	38.7	PM/PM10	52.0 lb/h	6.5519 g		PM/PM10	37.9	24.3	38.0	24.2	PM/PM10	38.0 lb/h	4.7879 g/s
SO2	6.1	6.2	3.0	3.0	SO2	6.2 lb/h	0.7771 g		SO2	13.2	10.2	13.1	10.0	SO2	13.2 lb/h	1.6630 g/s
ibient Temperature - 26 °	F								Ambient Temperature - 28 °F							
					Worst Case Paramet				Case Number:	3	9			Worst Case Paramet	ers	
Case Number:	· 4	10			yyorst Case Paramet	ura			Evap. Cooler	٠	•					
Evap. Cooler									Duct Burner Firing	×						
Duct Burner Firing	Х								Ouct parties runing	^						
					T 2 T	262.0 45	206 27 14		Exit Temp (°F)	167	179			Exit Temp	167.0 °F	348.15 K
Exit Temp (°F)	252	263			Exit Temp	252.0 °F	395.37 K		Exit Velocity (ft/s)	68	69			Exit Velocity	68.0 ft/s	20.7264 m/
Exit Velocity (ft/s)	81	82			Exit Velocity	81.0 ft/s	24.6888 m	ν5	Emissions (lb/h)	90	09			Emissions		
Emissions (lb/h)					Emissions	04 4 " "	10 2404		NOX	17.5	13.8			NOX	17.5 lb/h	2.2050 g/s
NOX	81.1	65.1			NOX	81.1 lb/h	10.2184 g		NOX CO	52.3	31.4			CO	52.3 lb/h	8.5897 g/s
CO	92.4	70.3			CO	92.4 lb/h	11.6422 g		PM/PM10	38.0	24.6			PM/PM10	38.0 lb/h	4.7879 g/s
PM/PM10	50.0 6.3	36.0			PM/PM10	50.0 lb/h	6.2999 g		SO2	13.6	10.7			502	13.6 lb/h	1.7189 g/s
SO2		3.1			SO2	6.3 lb/h	0.7921 g	1%	502	13.0	10.7					

NOx, lb/hr (w/ effects of SCR) CO, lb/hr PM₁₀, lb/hr (w/ effects of SO₁ oxidation)

SO₂, lb/hr (w/out effects of SO₂ oxidation)

# Appendix C Tanks Model Output

138859 C-1

# TANKS 4.0 Emissions Report - Detail Format Tank Identification and Physical Characteristics

Identification

User Identification: FT-001 City: Vero Beach State: Florida

Company: Florida Municipal Power Agency
Type of Tank: Vertical Fixed Roof Tank

Description: Treasure Coast Energy Center, Fuel Oil Storage Tank 001

**Tank Dimensions** 

 Shell Height (ft):
 40.00

 Diameter (ft):
 70.00

 Liquid Height (ft):
 35.00

 Avg. Liquid Height (ft):
 35.00

 Volume (gallons):
 1,000,000.00

 Turnovers:
 6.85

 Net Throughput (gal/yr):
 6,846,809.00

Is Tank Heated (y/n): N

**Paint Characteristics** 

Shell Cclor/Shade: White/White
Shell Condition: Good
Roof Color/Shade: White/White
Roof Condition: Good

**Roof Characteristics** 

Type: Dome

Height (ft): 0.00
Radius (ft) (Dome Roof): 70.00

**Breather Vent Settings** 

Vacuum Settings (psig): -0.03 Pressure Settings (psig): 0.03

Meteorological Data used in Emissions Calculations: Vero Beach, Florida (Avg Atmospheric Pressure = 14.75 psia)

# TANKS 4.0 Emissions Report - Detail Format Liquid Contents of Storage Tank

	***************************************				Liquid					····			.,,
			Daily Liquid Surf		Bulk				Vapor	Liquid	Vapor		
		Te	mperatures (deg	F)	Temp.	Vapor	Pressures (paia	)	Mol.	Mass	Mass	Mol.	Basis for Vapor Pressure
Mixture/Compor	ent Mont	h Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight	Fract,	Fract.	Weight	Calculations
. ,													
Distillate fuel oil	no. 2 All	74,17	69.18	79.18	72.43	0.0102	0.0087	0.0119	130.0000			188.00	Option 5: A=12.101, B=8907

# TANKS 4.0 Emissions Report - Detail Format Detail Calculations (AP-42)

Association Polarisation	
Annual Emission Calculations Standing Losses (lb):	106.5506
Vapor Space Volume (cu ft):	37,719.9454
Vapor Density (lb/cu ft):	0.0002
Vapor Space Expansion Factor:	0.0336
Vented Vapor Saturation Factor:	0.9947
Tomos Vapor Outstandin Deter-	
Tank Vapor Space Volume	
Vapor Space Volume (cu ft):	37,719.9454
Tank Diameter (ft):	70.0000
Vapor Space Outage (ft):	9.8013
Tank Shell Height (ft):	40.0000
Average Liquid Height (ft):	35.0000
Roof Outage (ft):	4.8013
Roof Outage (Dome Roof)	
Roof Outage (ff):	4,8013
Dome Radius (ft):	70.0000
Shell Radius (ft):	35.0000
Vepor Density (lb/ou ft):	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000
Vapor Pressure at Daily Average Liquid	755.5555
Surface Temperature (psia):	0.0102
Daily Avg. Liquid Surface Temp. (deg. R):	533.8411
Daily Average Ambient Temp. (deg. F):	72,4083
Ideal Ges Constant R	
(pale cuft / (fb-mot-deg R)):	10.731
Liquid Bulk Temperatura (deg. R):	532.0983
Tank Paint Solar Absorptance (Shell):	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700
Daily Total Solar Insulation	
Factor (Blu/sqft day):	1,304.2500
Vapor Space Expansion Factor	
Vapor Space Expansion Factor:	0.0336
Daily Vapor Temperature Range (deg. R):	18.9722
Dally Vapor Pressure Range (psis):	0.0032
Breather Vent Press. Setting Range(pala):	0.0800
Vapor Pressure at Daily Average Liquid	
Surfece Temperature (psie):	0.0102
Vapor Pressure at Dally Minimum Liquid	
Surface Temperature (psla):	0.0087
Vapor Pressure at Dally Maximum Uquid	
Surface Temperature (psia):	0.0119
Daily Avg. Liquid Surface Temp. (deg R):	533.8411
Daily Min. Liquid Surface Temp. (deg R):	528.8481
Daily Max. Liquid Surface Temp. (deg R):	538.8342
Daily Ambient Temp. Range (deg. R):	19.1167
Vented Vapor Saturation Factor	
Vented Vapor Saturation Factor:	0.9947
Vapor Pressure at Daily Average Liquid	
Surface Temperature (psia):	0.0102
Vapor Space Outage (ft):	9.8013

1/17/2005 11:45:13 AM

# TANKS 4.0 Emissions Report - Detail Format Detail Calculations (AP-42)- (Continued)

216.5159
130.0000
0.0102
6,846,809.000
0
6.8468
1.0000
1,000,000,000
0
35.0000
70.0000
1,0000

Total Losses (lb):

323.0665

# TANKS 4.0 Emissions Report - Detail Format individual Tank Emission Totals

## **Annual Emissions Report**

p - management and a second a second and a second a second and a second a second and a second an		Losses (lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	216.52	106.55	323.07

# **Appendix D**

Calculating Realistic PM₁₀ Emissions from Cooling Towers

Joel Reisman and Gordon Frisbie

Abstract 216

Air and Waste Management Association 94th Annual Conference and Exhibition in Orlando, Florida, June 25-28, 2001

# Calculating Realistic PM₁₀ Emissions from Cooling Towers

Abstract No. 216 Session No. AM-1b

#### Joel Reisman and Gordon Frisbie

Greystone Environmental Consultants, Inc., 650 University Avenue, Suite 100, Sacramento, California 95825

### **ABSTRACT**

Particulate matter less than 10 micrometers in diameter (PM₁₀) emissions from wet cooling towers may be calculated using the methodology presented in EPA's AP-42¹, which assumes that all total dissolved solids (TDS) emitted in "drift" particles (liquid water entrained in the air stream and carried out of the tower through the induced draft fan stack.) are PM₁₀. However, for wet cooling towers with medium to high TDS levels, this method is overly conservative, and predicts significantly higher PM₁₀ emissions than would actually occur, even for towers equipped with very high efficiency drift eliminators (e.g., 0.0006% drift rate). Such overprediction may result in unrealistically high PM₁₀ modeled concentrations and/or the need to purchase expensive Emission Reduction Credits (ERCs) in PM₁₀ non-attainment areas. Since these towers have fairly low emission points (10 to 15 m above ground), over-predicting PM₁₀ emission rates can easily result in exceeding federal Prevention of Significant Deterioration (PSD) significance levels at a project's fenceline. This paper presents a method for computing realistic PM₁₀ emissions from cooling towers with medium to high TDS levels.

### INTRODUCTION

Cooling towers are heat exchangers that are used to dissipate large heat loads to the atmosphere. Wet, or evaporative, cooling towers rely on the latent heat of water evaporation to exchange heat between the process and the air passing through the cooling tower. The cooling water may be an integral part of the process or may provide cooling via heat exchangers, for example, steam condensers. Wet cooling towers provide direct contact between the cooling water and air passing through the tower, and as part of normal operation, a very small amount of the circulating water may be entrained in the air stream and be carried out of the tower as "drift" droplets. Because the drift droplets contain the same chemical impurities as the water circulating through the tower, the particulate matter constituent of the drift droplets may be classified as an emission. The magnitude of the drift loss is influenced by the number and size of droplets produced within the tower, which are determined by the tower fill design, tower design, the air and water patterns, and design of the drift eliminators.

## AP-42 METHOD OF CALCULATING DRIFT PARTICULATE

EPA's AP-42¹ provides available particulate emission factors for wet cooling towers, however, these values only have an emission factor rating of "E" (the lowest level of confidence acceptable). They are also rather high, compared to typical present-day manufacturers' guaranteed drift rates, which are on the order of 0.0006%. (Drift emissions are typically

expressed as a percentage of the cooling tower water circulation rate). AP-42 states that "a conservatively high PM₁₀ emission factor can be obtained by (a) multiplying the total liquid drift factor by the TDS fraction in the circulating water, and (b) assuming that once the water evaporates, all remaining solid particles are within the PM₁₀ range." (Italics per EPA).

If TDS data for the cooling tower are not available, a source-specific TDS content can be estimated by obtaining the TDS for the make-up water and multiplying it by the cooling tower cycles of concentration. [The cycles of concentration is the ratio of a measured parameter for the cooling tower water (such as conductivity, calcium, chlorides, or phosphate) to that parameter for the make-up water.]

Using AP-42 guidance, the total particulate emissions (PM) (after the pure water has evaporated) can be expressed as:

For example, for a typical power plant wet cooling tower with a water circulation rate of 146,000 gallons per minute (gpm), drift rate of 0.0006%, and TDS of 7,700 parts per million by weight (ppmw):

PM =  $146,000 \text{ gpm x } 8.34 \text{ lb water/gal x } 0.0006/100 \text{ x } 7,700 \text{ lb solids/}10^6 \text{ lb water x } 60 \text{ min/hr} = <math>3.38 \text{ lb/hr}$ 

On an annual basis, this is equivalent to almost 15 tons per year (tpy). Even for a state-of-the-art drift eliminator system, this is not a small number, especially if assumed to all be equal to PM₁₀, a regulated criteria pollutant. However, as the following analysis demonstrates, only a very small fraction is actually PM₁₀.

## COMPUTING THE PM₁₀ FRACTION

Based on a representative drift droplet size distribution and TDS in the water, the amount of solid mass in each drop size can be calculated. That is, for a given initial droplet size, assuming that the mass of dissolved solids condenses to a spherical particle after all the water evaporates, and assuming the density of the TDS is equivalent to a representative salt (e.g., sodium chloride), the diameter of the final solid particle can be calculated. Thus, using the drift droplet size distribution, the percentage of drift mass containing particles small enough to produce PM₁₀ can be calculated. This method is conservative as the final particle is assumed to be perfectly spherical; hence as small a particle as can exist.

The droplet size distribution of the drift emitted from the tower is critical to performing the analysis. Brentwood Industries, a drift eliminator manufacturer, was contacted and agreed to provide drift eliminator test data from a test conducted by Environmental Systems Corporation (ESC) at the Electric Power Research Institute (EPRI) test facility in Houston, Texas in 1988 (Aull², 1999). The data consist of water droplet size distributions for a drift eliminator that achieved a tested drift rate of 0.0003 percent. As we are using a 0.0006 percent drift rate, it is reasonable to expect that the 0.0003 percent drift rate would produce smaller droplets, therefore,

this size distribution data can be assumed to be conservative for predicting the fraction of PM₁₀ in the total cooling tower PM emissions.

In calculating PM₁₀ emissions the following assumptions were made:

- Each water droplet was assumed to evaporate shortly after being emitted into ambient air, into a single, solid, spherical particle.
- Drift water droplets have a density  $(\rho_{\rm w})$  of water; 1.0 g/cm³ or 1.0 * 10⁻⁶  $\mu$ g /  $\mu$ m³.
- The solid particles were assumed to have the same density  $(\rho_{TDS})$  as sodium chloride, (i.e., 2.2 g/cm³).

Using the formula for the volume of a sphere,  $V = 4\pi r^3/3$ , and the density of pure water,  $\rho_w = 1.0 \text{ g/cm}^3$ , the following equations can be used to derive the solid particulate diameter,  $D_p$ , as a function of the TDS, the density of the solids, and the initial drift droplet diameter,  $D_d$ :

Volume of drift droplet = 
$$(4/3)\pi(D_a/2)^3$$
 [2]

Mass of solids in drift droplet = (TDS)(
$$\rho_{*}$$
)(Volume of drift droplet) [3]

substituting,

Mass of solids in drift = 
$$(TDS)(\rho_w)(4/3)\pi(D_d/2)^3$$
 [4]

Assuming the solids remain and coalesce after the water evaporates, the mass of solids can also be expressed as:

Mass of solids = 
$$(\rho_{TDS})$$
 (solid particle volume) =  $(\rho_{TDS})(4/3)\pi(D_p/2)^3$  [5]

Equations [4] and [5] are equivalent:

$$(\rho_{TDS})(4/3)\pi(D_p/2)^3 = (TDS)(\rho_w)(4/3)\pi(D_d/2)^3$$
 [6]

Solving for D_p:

$$D_{p} = D_{d} \left[ (TDS)(\rho_{w} / \rho_{TDS}) \right]^{1/3}$$
 [7]

Where,

TDS is in units of ppmw

 $D_p$  = diameter of solid particle, micrometers ( $\mu m$ )

 $D_d$  = diameter of drift droplet,  $\mu$ m

Using formulas [2] – [7] and the particle size distribution test data, Table 1 can be constructed for drift from a wet cooling tower having the same characteristics as our example; 7,700 ppmw TDS and a 0.0006% drift rate. The first and last columns of this table are the particle size distribution derived from test results provided by Brentwood Industries. Using straight-line interpolation for a solid particle size  $10 \, \mu m$  in diameter, we conclude that approximately  $14.9 \, percent$  of the mass emissions are equal to or smaller than  $PM_{10}$ . The balance of the solid

particulate are particulate greater than 10  $\mu$ m. Hence, PM₁₀ emissions from this tower would be equal to PM emissions x 0.149, or 3.38 lb/hr x 0.149 = 0.50 lb/hr. The process is repeated in Table 2, with all parameters equal except that the TDS is 11,000 ppmw. The result is that approximately 5.11 percent are smaller at 11,000 ppm. Thus, while total PM emissions are larger by virtue of a higher TDS, overall PM₁₀ emissions are actually lower, because more of the solid particles are larger than 10  $\mu$ m.

Table 1. Resultant Solid Particulate Size Distribution (TDS = 7700 ppmw)

EPRI Droplet	Droplet	Droplet Mass	Particle Mass	Solid Particle	Solid Particle	EPRI % Mass
Diameter	Volume	1	(Solids)	Volume	Diameter	Smaller
(µm)	(µm³)	( <i>µ</i> g) [3]	( _{AB} )	( _{1,000} )	(µm)	
	[2]'	<u> </u>	[4]		[7]	
10	524	5.24E-04	4.03E-06	1.83	1.518	0.000
20	4189	4.19E-03	3.23E-05	14.66	3.037	0.196
30	14137	1.41E-02	1.09E-04	49.48	4.555	0.226
40	33510	3.35E-02	2.58E-04	117.29	6.073	0.514
50	65450	6.54E-02	5.04E-04	229.07	7.591	1.816
60	113097	1.13E-01	8.71E-04	395.84	9.110	5.702
70	179594	1.80E-01	1.38E-03	628.58	10.628	21.348
90	381704	3.82E-01	2.94E-03	1335.96	13.665	49.812
110	696910	6.97E-01	5.37E-03	2439.18	16.701	70.509
130	1150347	1.15E+00	8.86E-03	4026.21	19.738	82.023
150	1767146	1.77E+00	1.36E-02	6185.01	22.774	88.012
180	3053628	3.05E+00	2.35E-02	10687.70	27.329	91.032
210	4849048	4.85E+00	3.73E-02	16971.67	31.884	92.468
240	7238229	7.24E+00	5.57E-02	25333.80	36.439	94.091
270	10305995	1.03E+01	7.94E-02	36070.98	40.994	94.689
300	14137167	1.41E+01	1.09E-01	49480.08	45.549	96.288
350	22449298	2.24E+01	1.73E-01	78572.54	53.140	97.011
400	33510322	3.35E+01	2.58E-01	117286.13	60.732	98.340
450	47712938	4.77E+01	3.67E-01	166995.28	68.323	99.071
500	65449847	6.54E+01	5.04E-01	229074.46	75.915	99.071
600	113097336	1.13E+02	8.71E-01	395840.67	91.098	100.000

Bracketed numbers refer to equation number in text.

The percentage of PM₁₀/PM was calculated for cooling tower TDS values from 1000 to 12000 ppmw and the results are plotted in Figure 1. Using these data, Figure 2 presents predicted PM₁₀ emission rates for the 146,000 gpm example tower. As shown in this figure, the PM emission rate increases in a straight line as TDS increases, however, the PM₁₀ emission rate increases to a maximum at around a TDS of 4000 ppmw, and then begins to decline. The reason is that at higher TDS, the drift droplets contain more solids and therefore, upon evaporation, result in larger solid particles for any given initial droplet size.

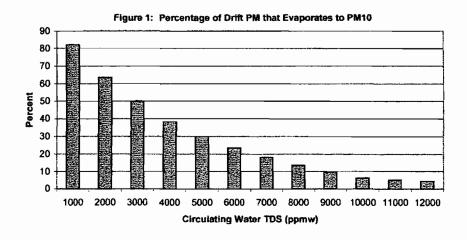
#### CONCLUSION

The emission factors and methodology given in EPA's AP-42¹ Chapter 13.4 Wet Cooling Towers, do not account for the droplet size distribution of the drift exiting the tower. This is a critical factor, as more than 85% of the mass of particulate in the drift from most cooling towers will result in solid particles larger than PM₁₀ once the water has evaporated. Particles larger than PM₁₀ are no longer a regulated air pollutant, because their impact on human health has been shown to be insignificant. Using reasonable, conservative assumptions and a realistic drift

droplet size distribution, a method is now available for calculating realistic PM₁₀ emission rates from wet mechanical draft cooling towers equipped with modern, high-efficiency drift eliminators and operating at medium to high levels of TDS in the circulating water.

Table 2. Resultant Solid Particulate Size Distribution (TDS = 11000 ppmw)

EPRI Droplet	Droplet	Droplet Mass	Particle Mass	Solid Particle	Solid Particle	EPRI % Mass
Diameter	Volume	()	(Solids)	Volume	Diameter	Smaller
(µm)	(µm³)	(Ag) [3]	(µg)	( _{µm} 3)	(µm)	
	[2]1		[4]		[7]	
10	524	5.24E-04	5.76E-06	2.62	1.710	0.000
20	4189	4.19E-03	4.61E-05	20.94	3.420	0.196
30	14137	1.41E-02	1.56E-04	70.69	5.130	0.226
40	33510	3.35E-02	3.69E-04	167.55	6.840	0.514
50	65450	6.54E-02	7.20E-04	327.25	8.550	1.816
60	113097	1.13E-01	1.24E-03	565.49	10.260	5.702
70	179594	1.80E-01	1.98E-03	897.97	11.970	21.348
90	381704	3.82E-01	4.20E-03	1908.52	15.390	49.812
110	696910	6.97E-01	7.67E-03	3484.55	18.810	70.509
130	1150347	1.15E+00	1.27E-02	5751.73	22.230	82.023
150	1767146	1.77E+00	1.94E-02	8835.73	25.650	88.012
180	3053628	3.05E+00	3.36E-02	15268.14	30.780	91.032
210	4849048	4.85E+00	5.33E-02	24245.24	35.909	92.468
240	7238229	7.24E+00	7.96E-02	36191.15	41.039	94.091
270	10305995	1.03E+01	1.13E-01	51529.97	46.169	94.689
300	14137167	1.41E+01	1.56E-01	70685.83	51.299	96.288
350	22449298	2.24E+01	2.47E-01	112246.49	59.849	97.011
400	33510322	3.35E+01	3.69E-01	167551.61	68.399	98.340
450	47712938	4.77E+01	5.25E-01	238564.69	76.949	99.071
500	65449847	6.54E+01	7.20E-01	327249.23	85,499	99.071
600	113097336	1.13E+02	1.24E+00	565486.68	102.599	100.000



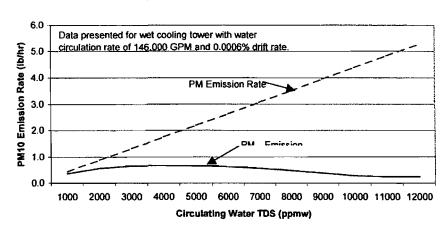


Figure 2: PM₁₀ Emission Rate vs. TDS

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#### **KEY WORDS**

Drift
Drift eliminators
Cooling tower
PM₁₀ emissions
TDS

# Appendix E Best Available Control Technology

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# Best Available Control Technology Analysis for Treasure Coast Energy Center Unit 1 Combined Cycle Combustion Turbine

#### Submitted by

Florida Municipal Power Agency

April 2005 Project No. 138859



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#### 1.0 Executive Summary

The 1977 Clean Air Act Amendment (CAAA) established revised conditions for the approval of preconstruction permit applications under the Prevention of Significant Deterioration (PSD) program. One of these requirements is that the best available control technology (BACT) be installed on new major sources or modifications to existing major sources for all pollutants regulated under the CAAA. Under the BACT process, the chosen technology cannot be less stringent than standards established by New Source Performance Standards (NSPS). The proposed Florida Municipal Power Agency (FMPA) Treasure Coast Energy Center (TCEC) Unit 1 includes one combined cycle combustion turbine with heat recovery steam generator (CTG/HRSG) that is subject to the BACT process. In addition, the Project will include an auxiliary boiler, safe shutdown diesel generator, mechanical draft cooling tower and emergency diesel engine fire pump. This document presents the BACT analysis and emissions control conclusions for the Project. The following is a summary of the proposed BACT determinations and associated emission rates for Unit 1, auxiliary boiler, safe shutdown diesel generator, mechanical draft cooling tower, and emergency diesel engine fire pump.

The Project will employ one GE Model PG7241 (FA) Combustion Turbine Generator (CTG) operating in combined cycle mode followed by a HRSG with supplemental duct burners. Unit 1 will fire natural gas primarily with up to 500 hours per year of ultra-low sulfur (ULS) fuel oil (0.0015 percent sulfur by weight) as a backup fuel. The duct burners will utilize only natural gas as the fuel source. Emissions for the BACT analysis are based on Unit 1 firing natural gas a maximum of 8,760 hours per year. The unit will operate between 40 and 100 percent of full load. The BACT analysis for Unit 1 resulted in the following determination:

- Nitrogen oxides (NO_x) emissions--BACT was determined to be the use of selective catalytic reduction (SCR) to achieve NO_x emissions of 2.0 ppmvd at 15 percent O₂ while firing natural gas and 8.0 ppmvd at 15 percent O₂ while firing ultra-low sulfur fuel oil.
- Carbon monoxide (CO) emissions--BACT analysis was determined to be the use of good combustion controls while firing natural gas or ultra-low sulfur fuel oil with less than 0.0015 percent sulfur by weight.
- Particulate (PM/PM₁₀) emissions--BACT was determined to be the use of good combustion controls and firing natural gas or ultra-low sulfur fuel oil with less than 0.0015 percent sulfur by weight.

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- Volatile organic compounds (VOC) emissions—The emissions of VOCs will be less than the major source PSD threshold level. Therefore a BACT analysis for VOCs is not required for Unit 1.
- Sulfur dioxide (SO₂) emissions--BACT was determined to be the use of natural gas and ultra-low sulfur fuel oil with less than 0.0015 percent sulfur by weight.
- Sulfuric acid mist (H₂SO₄) emissions--BACT was determined to be the use of good combustion controls while firing both natural gas and ultralow sulfur fuel oil with less than 0.0015 percent sulfur by weight.

The TCEC Unit 1 Project includes the installation of one 7.2 MBtu/h auxiliary boiler. The auxiliary boiler, utilized for support of the steam turbine generator, will fire only natural gas a maximum of 8,760 hours per year. BACT for the auxiliary boiler emissions was determined to be the use of good combustion controls while firing natural gas.

The TCEC Unit 1 Project includes the installation of one 500 kW safe shutdown diesel generator. The generator will utilize ultra-low sulfur fuel oil and will be employed on an emergency need basis. BACT for the safe shutdown diesel engine generator was determined to be the use of good combustion controls.

The TCEC Unit 1 Project includes the installation of one mechanical draft cooling tower. BACT for the mechanical draft cooling tower will be design of the cooling tower to minimize the cooling tower drift to less than 0.0005 percent of circulating water flow rate.

The TCEC Unit 1 Project includes the installation of one 300 hp emergency diesel engine fire pump. The fire pump will utilize ultra-low sulfur fuel oil and will be employed on an emergency need basis. BACT for the emergency diesel engine fire pump was determined to be the use of good combustion controls.

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#### 2.0 Project Description

Treasure Coast Energy Center Unit 1 (hereinafter referred to as Unit 1) to be installed by Florida Municipal Power Agency will consist of one GE Model PG7241 (FA) combustion turbine generator operating in combined cycle mode followed by a HRSG (CTG/HRSG).

The HRSG will utilize natural gas fired duct burners for supplemental heating of the flue gas for combined cycle operation.

The output rating of Unit 1 will be nominally 300 MW at 100 percent load and 73° F conditions. The proposed operating scenario for Unit 1 is 8,760 hours per year of natural gas operation with or without duct burner firing and up to 500 hours per year of operation on ultra-low sulfur fuel oil (combustion turbine only) with or without duct burner firing. The duct burners will fire only natural gas. The unit will be subject to frequent startups and will operate between 40 and 100 percent of full load. The duct burners in the HRSG will have a maximum rating of 545 MBtu/h (HHV) while firing natural gas at 100 percent load and 73° F conditions.

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#### 3.0 Basis of Unit 1 BACT Analysis

This section describes the basis for the Unit 1 BACT analysis. Information is provided on the BACT methodology and approach used as well as the parameters and factors used in developing the analysis. The following is a summary of the regulatory requirements and Project assumptions on which this BACT analysis is based.

#### 3.1 Regulatory and Methodology Basis

As defined in the air permit application, operation of Unit 1 will result in an increase in the potential to emit emissions of NO_x, CO, PM/PM₁₀, SO₂, and H₂SO₄ (sulfuric acid mist) in excess of the PSD significant emission rate threshold levels set for these pollutants. As required by PSD, for a new PSD major source, a BACT analysis is required for those pollutants with potential emission increases greater than the applicable PSD significant emission rate thresholds.

BACT is defined in Rule 62-210.200(37), F.A.C. as:

"Best Available Control Technology" or "BACT" – An emission limitation, including a visible emissions standard, based on the maximum degree of reduction of each pollutant emitted which the Department, on a case by case basis, taking into account energy, environmental and economic impacts, and other costs, determines is achievable through application of production processes, and available methods, systems and techniques (including fuel cleaning or treatment or innovative fuel combustion techniques) for control of each such pollutant."

However, BACT cannot be less stringent than the emissions limits established by an applicable New Source Performance Standard (NSPS), which for NO_x is 0.39 lb/MWh when firing natural gas and 1.2 lb/MWh when firing distillate oil. These limits are given in proposed NSPS Subpart KKKK, published in the February 18, 2005 Federal Register.

To bring consistency to the BACT process, the United States Environmental Protection Agency (USEPA) has authorized the development of a guidance document (March 15, 1990) on the use of the "top-down" approach to BACT determinations. The first step in a top-down BACT analysis is to determine, for the pollutant in question, the control technology alternatives that are technically feasible for the source category in question. Technologies required under the Lowest Achievable Emission Rate (LAER) for the source category must be considered when determining the control technology for the pollutant in question. LAER determinations, although not applicable to Unit 1, represent the top control alternatives under the BACT analysis process. A LAER determination would be required if Unit 1 was located in a non-attainment area.

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Federal and state ambient air quality standards, emission limitations, and other applicable regulations must be met by the technology chosen as BACT. The following criteria are given in Rule 62-212,400(6)(a), F.A.C.:

- "(6) Best Available Control Technology (BACT).
- (a) BACT Determination. Following receipt of a complete application for a permit to construct an air emissions unit or facility which requires a determination of Best Available Control Technology (BACT), the Department shall make a determination of Best Available Control Technology during the permitting process. In making the BACT determination, the Department shall give consideration to:
- 1. Any Environmental Protection Agency determination of Best Available Control Technology pursuant to Section 169 of the Clean Air Act, and any emission limitation contained in 40 CFR Part 60 (Standards of Performance for New Stationary Sources) or 40 CFR Part 61 (National Emission Standards for Hazardous Air Pollutants).
- 2. All scientific, engineering, and technical material and other information available to the Department.
- 3. The emission limiting standards or BACT determinations of any other state.
- 4. The social and economic impact of the application of such technology."

As previously noted, BACT cannot be less stringent than an applicable NSPS standard. The Federal NSPS for combustion turbines with an output greater than 1 MW (40 CFR 60 Subpart KKKK, proposed) establishes applicable NO_x and SO₂ emission limits or standards. No NSPS emission limits have been established for CO, PM/PM₁₀, or H₂SO₄. The following standards have been established by NSPS for Subpart KKKK units with an output greater than 30 MW:

- NO_x allowable limit = 0.39 lb/MWh when firing natural gas and 1.2 lb/MWh when firing distillate oil.
- SO₂ standard of 0.58 lb/MWh regardless of fuel/size or a fuel sulfur limit of 0.05 percent or less sulfur by weight.

#### 3.2 Operations/Emissions Basis

As mentioned previously, the proposed operating scenario for Unit 1 is a maximum 8,760 full load operating hours per year while firing natural gas with or without duct burner firing and a maximum of 500 hour per year while firing ultra-low sulfur distillate fuel oil with or without duct burner firing on natural gas. Table 3-1 shows the baseline emission rates for Unit 1 firing natural gas at 100 percent base load at an average annual site temperature of 73° F. The emissions shown in Table 3-1 are based on the use of dry low

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NO_x burners during natural gas firing using evaporative cooling and include emissions from the duct burners. The lb/MBtu values are based on the higher heating value (HHV) of the expected natural gas to be fired and are based on the combined heat input to the combustion turbine and the duct burners. This unit is expected to cycle with frequent startups and will be operated at 40 to 100 percent of full load for up to 8,760 hours per year.

Table 3-1 Baseline Emission Rates for Unit 1				
Emission Parameter	Unit 1 ^a Natural Gas, 100% Load, Duct Firing, Evaporative Cooling at a 73° F Ambient Temperature			
NO _x , ppmvd at 15% O ₂	12.2			
NO _x , lb/h	100.6			
NO _x , lb/Mbtu (HHV)	0.0444			
CO, ppmvd at 15% O ₂	8.0			
CO, lb/h	39.7			
CO, lb/Mbtu	0.0175			
PM/PM ₁₀ (front and back), lb/h ^b	35.8			
PM/PM ₁₀ (front and back), lb/Mbtu (HHV) ^b	0.0158			
SO ₂ , lb/h ^c	12.90			
SO ₂ , lb/Mbtu (HHV) ^c	0.0057			
H ₂ SO ₄ , lb/h ^b	3.47			
H ₂ SO ₄ , lb/Mbtu ^b	0.0015			

^aEmissions are based on firing natural gas in the CT and HRSG duct burners at 100 percent of base load with evaporative cooling at an ambient temperature of 73° F.

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^bPM/PM₁₀ and H₂SO₄ values include the affects of 20 percent SO₂ oxidation in the CT and 10 percent SO₂ oxidation in the duct burner.

^cSO₂ values do not include the effects of SO₂ oxidation.

#### 3.3 Economic Basis

The economic analyses used to determine the capital and annualized costs of the control technologies were based on USEPA methodologies shown in the USEPA "Best Available Control Technology Draft Guidance Document" (October 1990), "Top Down" Best Available Control Technology Guidance Document" (March 1990), The Office of Air Quality Planning and Standards (OAQPS) Control Cost Manual (February 1996, Fifth Edition), internal owner cost factors, and vendor budgetary cost quotes.

Table 3-2 lists the economic criteria used in the analysis of BACT alternatives. The capital recovery factor was calculated based on the present worth discount rate and economic life of the equipment or the assumed catalyst life.

Table 3-2 Project Economic Evaluation Criteria				
Economic Parameters	Value			
Contingency, percent	10			
Present Worth Discount Rate, percent	7.0			
Economic Life, years	20			
Capital Recovery Factor, (20 years)	0.0944			
SCR Catalyst Life, years	3			
SCONO _x Catalyst Life, years	5			
CO Catalyst Life, years	3			
Catalyst Capital Recovery Factor (3 years)	0.3811			
SCONO _x Catalyst Capital Recovery Factor (5 years)	0.2439			
Labor Cost, \$/man-hour	30			
Natural Gas Cost, \$/MBtu (2008)	5.47			
Aqueous Ammonia Cost, \$/ton (2004)	525			
Energy Cost, \$/kWh (2004)	0.0646			
Sales Tax, percent	N/A			

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#### 4.0 Unit 1 NO_x and CO BACT Analysis

The objective of this analysis is to determine the BACT for  $NO_x$  and CO emissions from Unit 1.

Unless otherwise noted, the emission rates described in this section are corrected to 15 percent oxygen.

#### 4.1 NO_x/CO BACT/LAER and Technology Review

A list of the top pertinent BACT/LAER decisions for NO_x is attached in Table A-1 of Appendix A. A review of the BACT/LAER documents (recent Florida permit actions; the California Air Pollution Control Officers Association, 1985 - 2004; and USEPA BACT/LAER Clearinghouse, 1990 - 2004) indicates that the lowest NO_x emissions permitted for a natural gas fired combustion turbine are 2.0 ppmvd for the facilities listed in Table A-1.

The Duke Energy Arlington Valley facility in Arlington, VA, is a recent project that was constructed as listed by the USEPA BACT/LAER Clearinghouse database. The facility consists of two gas fired combined cycle GE Frame 7FA gas turbines. The NO_x emissions are to be controlled by dry low NO_x combustors and selective catalytic reduction (SCR). The units have been permitted at 2.0 ppmvd at 15 percent O₂ with an ammonia slip of 10 ppmvd at 15 percent O₂.

The FPL Turkey Point combined cycle units project in Florida is a recent project that was issued a final permit by the FDEP on February 8, 2005. The project consists of four gas fired combined cycle GE 7FA turbines/HRSGs with duct burner firing. The NO_x emissions are to be controlled by dry low NO_x combustors and selective catalytic reduction (SCR). The units have been permitted at 2.0 ppmvd at 15 percent O₂ with an ammonia slip of 5 ppmvd at 15 percent O₂.

For CO, a list of the top pertinent BACT/LAER decisions is attached in Table A-2 of Appendix A. A review of the BACT/LAER Clearinghouse documents indicates that the most stringent CO emission level for a combustion turbine is 1.8 ppmvd at 15 percent O₂ for the Newark Bay Cogeneration L.P. project located in New Jersey. The 49.5 MW SW 251 B11/12 Siemens-Westinghouse combustion turbine units fire natural gas. The low emissions are achieved by reducing CO emissions by 80 percent (from 9 ppmvd to 1.8) through the use of an oxidation catalyst. It should be noted that the Newark Bay project, which is located in a non-attainment area for CO, represents LAER.

A summary of recent NOx and CO BACT determinations for EPA Region 4 is included as Tables A-3 and A-4, respectively, in Appendix A. These tables were generated using the National Combustion Turbine Spreadsheet maintained by EPA

Region 4. The information in the National Combustion Turbine Spreadsheet was filtered to only show determinations made in Region 4 for combined cycle combustion turbines.

#### 4.2 Alternative NO_x Emission Reduction Systems

During combustion,  $NO_x$  is formed from two sources.  $NO_x$  emissions formed through the oxidation of the fuel bound nitrogen are called fuel  $NO_x$ .  $NO_x$  emissions formed through the oxidation of a portion of the nitrogen contained in the combustion air are called thermal  $NO_x$  and are a function of combustion temperature.  $NO_x$  production in a gas turbine combustor occurs predominantly within the flame zone, where localized high temperatures sustain the  $NO_x$ -forming reactions. The overall average gas temperature required to drive the turbine is well below the flame temperature, but the flame region is required to achieve stable combustion.

Nitrogen oxide control methods may be divided into two categories: in-combustor  $NO_x$  formation control and post-combustion emission reduction. An in-combustor  $NO_x$  formation control process reduces the quantity of  $NO_x$  formed in the combustion process. A post-combustion technology reduces the  $NO_x$  emissions in the flue gas stream after the  $NO_x$  has been formed in the combustion process. Both of these methods may be used alone or in combination to achieve the various degrees of  $NO_x$  emissions required. The six different types of emission controls reviewed by this BACT analysis are as noted below.

- In-Combustor Type:
  - Water/Steam Injection.
  - Dry Low-NO_x (DLN) Burners.
  - Xonon.
- Post-Combustion Type:
  - Selective Non-Catalytic Reduction (SNCR).
  - SCONO_x.
  - Selective Catalytic Reduction (SCR).

The rationale behind whether the above technologies are evaluated as NO_x control for BACT is included in the following subsections.

#### 4.2.1 Water or Steam Injection

 $NO_x$  emissions from Unit 1 can be controlled by either water or steam injection. This type of control injects water or steam into the primary combustion zone with the fuel. The water or steam serves to reduce  $NO_x$  formation by reducing the peak flame temperature. The degree of reduction in  $NO_x$  formation is proportional to the amount of water injected into the combustion turbine. A limit exists, however, on the amount of water that can be injected into the system before reliability of the combustion turbine is

seriously degraded and operational life is affected. This type of control can also be counterproductive with regard to CO and VOC emissions that are formed as a result of incomplete combustion.

The development of dry low-NO_x burners has replaced the use of wet controls, except for certain cases, such as oil firing. Since Unit 1 will fire natural gas as the primary fuel with ultra-low sulfur fuel oil as a back up, water injection will only be used during oil firing and will not be evaluated for the primary operating case of natural gas.

#### 4.2.2 Dry Low-NO_x Burners

 $NO_x$  formation can be limited by lowering combustion temperatures and by staging combustion (i.e., creating a reducing atmosphere followed by an oxidizing atmosphere). The use of dry low- $NO_x$  (DLN) burners as a way to reduce flame temperature is one common  $NO_x$  control method. These combustor designs are called DLN burners because, when firing natural gas, injecting water into the combustion chamber is not necessary to achieve low  $NO_x$  emissions. Most industry gas turbine manufacturers today have developed this type of lean premix combustion system as the state of the art for  $NO_x$  controls in combustion turbines. This method is exclusively utilized when firing natural gas. This technology will form the base case for the BACT analysis.

#### **4.2.3 XONON**

Another form of in-combustor control is XONON. This technology, developed by Catalytica Combustion Systems, is designed to avoid the high temperatures created in conventional combustors. The XONON combustor operates below 2,700° F at full power generation, which significantly reduces NO_x emissions without raising, and possibly even lowering, emissions of CO and unburned hydrocarbons. XONON uses a proprietary flameless process in which fuel and air react on the surface of a catalyst in the turbine combustor to produce energy in the form of hot gases, which drive the turbine. This emerging technology is being commercialized by several joint ventures that Catalytica has with turbine manufacturers.

Although this technology has been applied to small turbines, such as a Kawasaki M1A-13X (1.5 MW) combustion turbine, it has not been applied to utility size combustion turbines such as proposed for Unit 1. It is expected that application of this technology to utility size combustion turbines will require a period of "scale up" and testing before it can be determined that this technology can demonstrate in practice a given NO_x emission limit. Because this technology has not been applied to utility size combustion turbines firing natural gas, it is not considered to be technically feasible for

Unit 1. As such, this method of combustion control will be eliminated from further evaluation for control of  $NO_x$  emissions in this BACT analysis.

#### 4.2.4 Selective Non-Catalytic Reduction

Selective non-catalytic reduction (SNCR) is one method of post-combustion control. SNCR selectively reduces NO_x into nitrogen and water vapor by reacting the flue gas with a reagent. The SNCR system is dependent upon the reagent injector location and temperature to achieve proper reagent/flue gas mixing for maximum NO_x reduction. SNCR systems require a fairly narrow temperature range for reagent injection in order to achieve a specific NO_x reduction efficiency. The optimum temperature range for injection of ammonia or urea is 1,500° to 1,900° F. The NO_x reduction efficiency of an SNCR system decreases rapidly at temperatures outside the optimum temperature window. Operation below this temperature window results in excessive ammonia emissions (ammonia slip). Operation above the temperature window results in increased NO_x emissions.

Because the exhaust temperature at the exit of the combustion turbine proposed for this project (approximately 1,200° F) is less than the optimum temperature range for the application of this technology, it is not technically feasible to apply this technology to this Project and it will be eliminated from further evaluation in this BACT analysis.

#### 4.2.5 SCONOx

A second, relatively new post-combustion technology from Goal Line Environmental Technologies in conjunction with ABB Alstom Power is SCONO_x, which utilizes a coated oxidation catalyst to remove both NO_x and CO without a reagent such as ammonia.

The SCONO_x system utilizes hydrogen (H₂) (which is created by reforming natural gas) as the basis for a proprietary catalyst regeneration process. The system consists of a platinum-based catalyst coated with potassium carbonate (K₂CO₃) to oxidize both NO_x and CO, thereby reducing total plant emissions. CO emissions are decreased by the oxidation of CO to carbon dioxide (CO₂). The catalyst is installed in the flue gas at a point where the temperature is between 300° to 700° F. ABB Alstom/Goal Line guarantees the performance of the catalyst for 3 years. When the catalyst reaches the end of its service life, it can be recycled to recover the precious metal contained within the catalyst.

The SCONO_x catalyst is very susceptible to fouling by sulfur in the flue gas. The impact of sulfur can be minimized by a sulfur absorption SCOSO_x catalyst. The SCOSO_x catalyst is located upstream of the SCONO_x catalyst. The SO₂ is oxidized to sulfur

trioxide (SO₃) by the SCOSO_x catalyst. The SO₃ is then deposited on the catalyst and removed from the catalyst when it is regenerated. The SCOSO_x catalyst is regenerated along with the SCONO_x catalyst.

The SCONO_x catalyst will require that it be re-coated or "washed" every 6 months to 1 year. The frequency of washing is dependent on the sulfur content in the fuel and the effectiveness of the SCOSO_x catalyst. The "washing" consists of removing the catalyst modules from the unit and placing each module in a potassium carbonate reagent tank, which is the active ingredient of the catalyst. The SCOSO_x catalyst will also require washing, but due to limited operating experience with the SCOSO_x catalyst, it is uncertain how often this will be required. However, it is expected that the SCOSO_x catalyst will require annual washing.

The current SCONO_x catalyst technology is in its second generation. The first generation operated for approximately 10 months on a small LM-2500 combined cycle combustion turbine unit before the SCONO_x system was taken out of service because of poor regeneration gas distribution.

The USEPA has stated its concerns (November 19, 1999 letter from USEPA Region I) with the technical uncertainties of the SCONO_x system and was apprehensive about applying SCONO_x technology to large combined cycle turbines that burn primarily natural gas. The combustion turbine proposed for this project is approximately 170 MW, which is outside the operating range (32 MW) of the SCONO_x system currently operating at the Federal Cold Storage Cogeneration facility in California.

As discussed above, the SCONO_x technology may have future promise. The application of this technology is currently limited to natural gas combined cycle combustion turbine units under 40 MW. However in the interest of providing a complete technology analysis, SCONO_x will be evaluated in the BACT for NO_x control.

#### 4.2.6 Selective Catalytic Reduction

Another post-combustion method of NO_x control is selective catalytic reduction (SCR). SCR systems have been used quite extensively in CTG/HRSG projects for the past ten years. The SCR process combines vaporized ammonia with NO_x in the presence of a catalyst to form nitrogen and water. The vaporized ammonia is injected into the combustion turbine exhaust gases prior to passage through the catalyst bed. The use of SCR results in small levels of ammonia emissions (ammonia slip). As the catalyst degrades ammonia slip will increase to approximately 5 -10 ppmvd (dependent on system design), ultimately requiring catalyst replacement.

The performance and effectiveness of SCR systems are directly dependent on the temperature of the flue gas when it passes through the catalyst. Vanadium/titanium catalysts have been used on the majority of SCR system installations. The flue gas temperature range for optimum SCR operation using a conventional vanadium/titanium

catalyst is approximately 600 to 750° F. At temperatures above 850° F permanent damage to the vanadium/titanium catalyst occurs. For Unit 1, the flue gas temperature in the HRSG of the CTG/HRSG would typically range from 600° F to 800° F. Accordingly, a vanadium/titanium catalyst can be installed for Unit 1. Therefore, the vanadium/titanium-based catalyst will be evaluated further for these units.

Because the SCR system requires the regulation of ammonia injection based on the NO_x emission monitors, the accuracy of the emission reading directly influences the amount of actual error in the ammonia injection rate. Therefore, erroneous emission readings can result in excess ammonia levels even when the actual NO_x value is below the permitted value. This may result in excessive ammonia "slip" being discharged to the atmosphere with little or no improvement in NO_x emissions. Reduction of the NO_x emission concentrations to levels below 2.0 ppmvd also raises concerns with the additional ammonia that may be emitted to obtain further reduced levels. Although SCR catalyst vendors have indicated that ammonia emissions will not be increased, these vendors are not solely responsible for guaranteeing ammonia slip. The distribution of the ammonia in the duct is the key parameter since localized maldistribution of the ammonia will cause the ammonia to pass through the catalyst without reacting with the NO_x. The proper distribution of the gas and ammonia is difficult to obtain when both reactants, NO_x and NH₃, are at such low concentrations. This distribution would be even more difficult, if not impossible, to maintain during transient operations, such as load changes, when flow patterns are changing. Changes in operation from one stable load to another stable load may present problems since the flow patterns and the loads may be different. Since the catalyst vendors are not responsible for the ammonia distribution, they typically limit their guarantees to some distribution level. Such conditions to reduce NO_x emissions to levels below 2.0 ppmvd that increase ammonia emissions will be counter productive to the reduction of overall emissions since ammonia presents an emission problem itself.

This SCR method of post-combustion control will be considered in this BACT analysis to control NO_x emissions.

#### 4.2.7 NO_x Control Summary

This technology evaluation indicates that an SCR and a SCONO_x system are the control technologies suitable for further evaluation beyond the use of good combustion practices, as provided by a DLN burner, and will be considered in this BACT analysis.

#### 4.3 Alternative CO Emission Reduction Systems

Typically, measures taken to minimize the formation of NO_x during combustion inhibit complete combustion, which increase the emissions of CO. Carbon monoxide is

formed during the combustion process due to incomplete oxidation of the carbon contained in the fuel. CO formation is limited by ensuring complete and efficient combustion of the fuel in the combustion turbine. High combustion temperatures, adequate excess air, and good air/fuel mixing during combustion minimize CO emissions.

Carbon monoxide control methods may be divided into two categories: incombustor CO formation control and post-combustion emission reduction. An incombustor CO formation control process minimizes the quantity of CO formed in the combustion process. A post-combustion technology reduces the CO emissions in the flue gas stream after the CO has been formed in the combustion process. Both of these methods may be used alone or in combination to achieve the various degrees of CO emissions required. The three different types of emission controls reviewed by this BACT analysis are as noted below.

- In-Combustor Type:
  - Dry Low-NO_x (DLN) Burners.
- Post-Combustion Type:
  - Oxidation Catalyst.
  - SCONO_x.

The rationale behind whether the above technologies are evaluated as CO control for BACT is included in the following subsections.

#### 4.3.1 Dry Low-NO_x Burners and Good Combustion Control

The development of good combustion practice improvements with state of the art DLN burners has reduced CO emissions as compared to those previously obtained by the use of water injection as the main NO_x control method. These improved combustion characteristics have allowed minimization of CO emissions without sacrificing NO_x control performance. For this reason, the use of low NO_x burners that use good combustion practices is the standard method of also controlling CO emissions.

#### 4.3.2 CO Oxidation Catalyst

A current CO reduction technology available that will not impact  $NO_x$  emissions is the use of an oxidation catalyst to convert the CO to  $CO_2$ . The oxidation catalyst is typically a precious metal catalyst. None of the catalyst components are considered toxic. No reagent injection is necessary and oxidizing catalysts, dependent on the uncontrolled emission level, are capable of reducing CO emissions from 80 to 90 percent. An 77.5 percent CO reduction rate (i.e. 8 ppm to 1.8 ppm)has been assumed for this BACT analysis.

#### 4.3.3 SCONO_x

Another CO control technology that was previously discussed for NO_x control is the SCONO_x process. The SCONO_x system reduces CO emissions by oxidizing the CO to CO₂. The demonstrated application for this technology is currently limited to combined cycle combustion turbine units under 40 MW. The combustion turbine proposed for this project is approximately 170 MW, which is outside the operating range (32 MW) of the SCONO_x system currently operating at the Federal Cold Storage Cogeneration facility in California.

As discussed above, the SCONO_x technology may have future promise. The application of this technology is currently limited to natural gas combined cycle combustion turbine units under 40 MW. However in the interest of providing a complete technology analysis, SCONO_x will be evaluated in the BACT for CO control. Based on previous removal rates proposed by Goal Line, as with the CO Oxidation catalyst, 77.5 percent reduction rate has been assumed for this BACT analysis.

#### 4.3.4 CO Control Technology Summary

This technology evaluation indicates that an oxidation catalyst and a SCONO_x system are the control technologies suitable for further evaluation beyond the use of good combustion practices, as provided by a DLN burner, and will be considered in this BACT analysis.

#### 4.4 Combined NO_x and CO Control Technology Summary

In-combustor NO_x and CO control by advanced combustion controls using dry low NO_x burners is the least stringent control technology considered for Unit 1. However, the use of a combination SCR/oxidation catalyst system or the SCONO_x system are technologies capable of achieving significantly lower emissions than the application of dry low NO_x burners alone. Because the SCONO_x system is capable of reducing NO_x and CO, emissions, the NO_x and CO BACT analyses have been combined to avoid double counting the SCONO_x technology, thus inflating its economic impacts. The following control technologies will be evaluated in this BACT analysis and are ranked in order of relative control effectiveness:

In-combustor NO_x and CO control consisting of DLN combustors to limit outlet emissions during natural gas firing for all operating loads for Unit 1 is considered the base case scenario. All modern combustion turbines of the type proposed for this Project include DLN combustors.

- The addition of an SCR system and oxidation catalyst to reduce outlet NO_x emissions from the natural gas fired CTG/HRSG with duct burner to the level of 2.0 ppmvd and CO to 1.8 ppmvd emissions for the natural gas fired CTG/HRSG with duct burners.
- The addition of a SCONO_x system to reduce outlet NO_x emissions from the natural gas fired CTG/HRSG with duct burner to the NO_x level of 2.0 ppmvd and CO emissions to 1.8 ppmvd.

The following evaluation considers energy, environmental, and economic impacts for the NO_x and CO combined technology scenarios evaluated. Table 4-1 outlines the expected NO_x and CO emissions rates from the evaluated emissions control alternatives of dry low NO_x burners (i.e. good combustion controls), SCR/CO catalyst, and SCONO_x. SCR/CO catalyst and SCONO_x are considered the most stringent NO_x and CO emissions control alternatives as they achieve the lowest outlet emission rate. Therefore, if SCONO_x is not found viable via energy, environmental, or economic impacts for the combined emissions reduction, the SCONO_x technology will be eliminated from consideration, and a BACT evaluation would be done for control of NO_x and CO emissions separately.

## 4.5 NO_x and CO Combined Technology Energy, Environmental, and Economic Impacts Evaluation

The following section identifies the energy, environmental and economic impacts of the NO_x and CO combined control technologies.

#### 4.5.1 SCONO_x Energy Impacts

The use of a SCONO_x system will increase the energy requirements on the system compared to use of dry low NOx burners alone. The SCONOx system will increase the backpressure on the combustion turbine by about 4 inches water gauge (in. w.g.). This will reduce the output of Unit 1 by approximately 0.3 percent and increase the lost power generation. In addition, the period required for catalyst washing will result in increasing the lost power generation. Wahlco-Metroflex estimated the unit will be offline for a 24 hour period once per year to accommodate the washing process. Furthermore, there will be an energy loss due to steam consumption from the regeneration system. Steam is used as the carrier medium for the regeneration gas for the SCONO_x system. Wahlco-Metroflex estimated that approximately 5,000 lb/h of steam would be used in the regeneration production. These three effects will be added together to determine the total lost power generation and are included in the annualized cost estimate. The SCONO_x system will have minimal effect on power consumption that will be necessary to operate the damper actuators and regeneration system. Wahlco-Metroflex estimated that approximately 15 kW would be consumed during operation of the SCONO_x system. This

Table 4-1
Estimated NO_x and CO Emissions from Alternate Control
Technologies for Unit 1

Control Technology Alternatives					
LNB/Good Combustion Controls	Combustion SCR/CO				
12.2	2.0	2.0			
100.6	16.5	16.5			
440.6	72.3	72.3			
N/A	83.6%	83.6%			
Base	368.3	368.3			
8.0	1.8	1.8			
39.7	8.9	8.9			
173.9	39.1	39.1			
N/A	77.5%	77.5%			
Base	134.8	134.8			
	LNB/Good Combustion Controls 12.2 100.6 440.6 N/A Base 8.0 39.7 173.9 N/A	LNB/Good Combustion Controls       SCR/CO Catalyst         12.2       2.0         100.6       16.5         440.6       72.3         N/A       83.6%         Base       368.3         8.0       1.8         39.7       8.9         173.9       39.1         N/A       77.5%			

^aTotal emissions are based on 8,760 hours per year firing natural gas at an ambient temperature of 73° F.

increase in power consumption will be included in the annualized cost estimate. The natural gas required for the production of the regeneration gas will increase the annualized cost associated with using the SCONO_x system. The annualized cost of natural gas consumption is included in the annualized cost analysis.

#### 4.5.2 SCONO_x Environmental Impacts

The SCONO_x catalyst is composed of precious metals coated with potassium carbonate. When the potassium carbonate coating can no longer be regenerated, the precious metal content of the remaining catalyst can be recycled. Although recycling the potassium carbonate is a positive aspect of this technology, the oxidation of CO and VOC that results from the application of this technology directly results in an increased production of CO₂, a greenhouse gas. There is currently a worldwide effort to reduce industrial emissions of CO₂ because of its contribution to global climate change. Installation of a SCONO_x system would directly counter this initiative.

The SCONO_x catalyst will oxidize approximately 1.0 percent of the  $SO_2$  in the flue gas to  $SO_3$ . The  $SO_3$  will then react with the moisture in the flue gas to form sulfuric acid mist in the atmosphere. Any sulfuric acid mist formed will increase the amount of particulate matter emitted in the flue gas. The particulate matter will predominately consist of  $PM_{10}$ .

#### 4.5.3 SCR Energy Impacts

The use of an SCR system impacts the energy requirements of Unit 1. An SCR system requires an ammonia storage, handling and delivery system, which would include vaporizers and blowers to vaporize and dilute the ammonia reagent for injection. In addition, an SCR system catalyst would increase the backpressure on the combustion turbine. The SCR system would add about 2.8 inches water gauge (in. w.g.) backpressure to the unit for the NO_x reduction to 2.0 ppmvd. This would reduce the output of Unit 1 by approximately 516 kW.

#### 4.5.4 SCR Environmental Impacts

The vanadium content of the SCR catalyst contributes to its classification as a hazardous waste. Therefore, spent catalyst may need to be handled and disposed of following hazardous waste procedures. Because of this, recycling of SCR catalysts for vanadium has become common.

The use of ammonia in an SCR system introduces an element of environmental risk. Ammonia is listed as a hazardous substance under Title III Section 302 of the Superfund Amendments and Reauthorization Act of 1986 (SARA). However, the storage and use of

ammonia has been a relatively routine practice in utility power plants and industrial plant processes and is also regulated by USEPA's Chemical Accident Prevention Provisions. This BACT analysis is based on the use of aqueous ammonia that can be stored and used more safely than anhydrous ammonia. According to the Committee on Toxicology of the National Academy of Sciences and the Committee on Medical and Biological Effects of Environmental Pollutants (both of the National Research Council), the following threshold concentrations exist for ammonia:

Human Response	Concentration (ppm)
Immediate throat irritation	Equal to or greater than 400
Eye irritation	Equal to or greater than 700
Coughing	Equal to or greater than 1,700
Life threatening for short exposure	2,500 to 6,500
Rapidly fatal for short exposure	5,000 to 10,000

Some ammonia slip from the Combustion Turbine Unit 1 stack is unavoidable due to the imperfect distribution of the reagent and catalyst deactivation. Although ammonia emissions are not regulated nationally, the Northeast States for Coordinated Air Use Management (NESCAUM) has recommended an ammonia slip emissions limit of 10 ppmvd, unless that limit is shown to be inappropriate. Ammonia slip from an SCR system is one of the major design consideration that establishes catalyst life. Therefore, lower ammonia slip requirements ultimately limit catalyst life and dictate associated catalyst replacement. Exceeding the NESCAUM's recommendation, FDEP recently proposed an ammonia slip of 5 ppmvd for Turkey Point, a combined cycle combustion turbine unit utilizing SCR. Based on the recent Turkey Point air permit, an ammonia slip design value of 5 ppmvd at 15 percent O₂ is used for this analysis.

The SCR catalyst will oxidize approximately 2 to 3 percent of the SO₂ in the flue gas to SO₃. Once the flue gas cools below approximately 600° F, the ammonia present in the flue gas may react with SO₃ to form ammonium sulfate and bisulfate salts. This formation may be dependent on the particular plume dispersion characteristics at the given time of stack discharge, which is dependent upon the temperature reached once the flue gas has left the stack. However, if the ammonia sulfate compounds are not formed, the SO₃ will react with the moisture in the flue gas to form sulfuric acid mist in the atmosphere. Any ammonium sulfate and bisulfate salts and sulfuric acid mist formed will increase the amount of particulate matter emitted in the flue gas. The particulate material will predominately consist of matter less than PM₁₀. As the catalyst gradually deactivates, more ammonia must be injected to compensate and maintain the desired NO_x reduction. This results in an increased amount of ammonia slip for a given level of

performance. Increased ammonia slip in turn results in additional ammonia salt formation which could result in increased opacity and particulate emissions from Unit 1.

#### 4.5.5 Oxidation Catalyst Energy Impacts

An oxidation catalyst reactor located downstream of the combustion turbine exhaust will increase the backpressure on the combustion turbine. The additional backpressure of about 1.2 inches, water gauge, will reduce the combustion turbine output by approximately 221 kW. The cost of lost power revenue due to the backpressure is included in the economic analysis.

#### 4.5.6 Oxidation Catalyst Environmental Impacts

The major environmental disadvantage that exists when using an oxidation catalyst to reduce CO emissions is that a percentage of the SO₂ in the flue gas will oxidize to SO₃. The higher the operating temperature, the higher the SO₂ to SO₃ oxidation potential. It is estimated that approximately 20 percent of the SO₂ in the flue gas will oxidize to SO₃ as a result of the oxidation catalyst being installed after the combustion turbine outlet with high temperatures. The SO₃ will react with the moisture in the flue gas to form sulfuric acid mist (H₂SO₄). The increase in H₂SO₄ emissions would increase PM₁₀ emissions.

Spent oxidation catalyst is made up of precious metals that are not considered toxic. This allows the catalyst to be handled and disposed of following normal waste procedures. Because of the precious metal content of the catalyst, the oxidation catalyst can also be recycled to recover the precious metals.

As mentioned previously, the installation of an oxidation catalyst will also increase the backpressure on the turbine, thereby decreasing efficiency. This decrease in efficiency will lead to increased emissions of all pollutants on a unit power output basis. The oxidation of CO also directly results in increased production of CO₂, a greenhouse gas. There is currently a worldwide effort to reduce industrial emissions of CO₂ because of its contribution to global climate change. Installation of an oxidation catalyst would directly counter this initiative.

### 4.5.7 Economic Impacts for SCR (2.0 ppmvd)/Oxidation Catalyst Versus SCONO_x

The use of an SCR/oxidation catalyst or SCONO_x has significant economic impacts to Unit 1. An analysis of the economic impact is provided in this section.

**4.5.7.1** Capital Costs for SCR (2.0 ppmvd)/Oxidation Catalyst and SCONO_x. Table 4-2 presents the capital costs for installing an SCR/oxidation catalyst and SCONO_x

Table 4-2
NO_x/CO Combined Control Alternative Capital Cost For Unit 1

			<u> </u>	
	DLN	SCONO _x	SCR/OX Cat	Remarks
Direct Capital Cost		_		Cost based on emissions in Table 4-1
Catalysts	N/A	Included	1,436,000	Estimated from NE Corporation
Catalyst Reactor Housing	N/A	Included	604,000	Estimated from previous projects
SCONO _x System	N/A	7,800,000	0	Vendor Estimate
Control/Instrumentation	N/A	180,000	180,000	Estimated; includes controls and monitoring equipment.
Ammonia (Storage & Injection/Dilution)	N/A	N/A	420,000	Estimated from Peerless Mfg. Co and previous projects.
Purchased Equipment Costs (PEC)	N/A	7,980,000	2,640,000	
Sales Tax		0	0	Not applicable to FMPA
Freight	N/A	798,000	264,000	10% of PEC
Balance of Plant	N/A	2,394,000	792,000	30% of PEC. See text for background information on this item
Total Direct Cost (DC)	N/A	11,172,000	3,696,000	
Indirect Capital Costs				
Contingency	N/A	1,117,000	370,000	10% of DC
Engineering and Supervision	N/A	1,117,000	370,000	10% of DC for SCONO _x . 10% of DC for SCR and 10% of DC for CO catalyst.
Construction & Field Expense	N/A	559,000	185,000	5% of DC
Construction Fee	N/A	1,117,000	370,000	10% of DC
Start-up Assistance	N/A	223,000	74,000	2% of DC
Performance Test	N/A	50,000	50,000	Assumed \$50,000 emission test.
Total Indirect Capital Costs (IC)	Base	4,183,000	1,419,000	
Installed Costs (DC+IC)	Base	15,355,000	5,115,000	
Less Catalyst	Base	4,800,000	1,436,000	Catalyst is viewed as an O&M value.
Total Capital Investment (TCI)	Base	10,555,000	3,679,000	TCI = DC + IC – Catalyst

system on Unit 1 during natural gas firing to achieve a NO_x outlet emission level of 2.0 ppmvd and a CO outlet emission rate of 1.8 ppmvd. The cost of the SCR/oxidation catalyst system includes the ammonia receiving, storage, transfer, vaporization, and injection; catalytic reactor housing; controls and instrumentation and freight. The catalyst costs were not included in the total capital investment (TCI) cost but assessed as an annual cost. The cost of the SCONO_x system includes the catalyst, regenerative gas distribution system, catalytic reactor housing, controls and instrumentation, and freight. The BOP cost for the SCR/oxidation catalyst and SCONO_x system consist of 8 percent of the purchased equipment costs (PEC) for foundation and supports, 14 percent for handling and erection, 4 percent for electrical installation, 2 percent for piping, 1 percent for insulation, and 1 percent for painting. Capital costs were based on budgetary quotations from equipment manufacturers and other engineering estimates.

Quotations for the SCR and oxidation catalyst material were based on vanadium/titanium and precious metal type catalysts, respectively. The direct installation costs included the balance of plant items such as foundations, insulation and lagging and painting and were calculated as percentages of the total purchased equipment costs. The total capital investment was calculated as the summation of the total direct cost (DC) and total indirect costs (IC) per OAQPS cost methods. The indirect capital costs for the SCR/Oxidation Catalyst systems are percentages of the total direct costs (DC) and are site specific. The indirect capital costs for the SCONO_x system are percentages of the SCONO_x system DC.

There are many potential items and uncertainties that are not captured by the cost items included in the estimate, such as possible changes between cost quotes and contract values, changes in operating conditions, process contingency, increased equipment cost, scope changes, labor/wage increases, and schedule acceleration. In addition, the Electric Power Research Institute published the document titled, NO_x Emissions: Best Available Control Technology, A Gas Turbine Permitting Guidebook in November 1991 and list under NO_x control cost (Page 5-5) the following text:

"Based on experience with other cost methodology sources, the contingency factor recommended by the OAQPS Manual (3% of the total equipment cost) is a lower-bound estimate. Standard EPA guidance for pollution control costing is a contingency factor of 10 to 50% of the sum of direct and indirect costs.\(^1\) A contingency factor of 20% of the sum of direct and indirect costs was used in the economic analyses conducted by the EPA in support of the NSPS for industrial and

¹U.S. Environmental Protection Agency, A Standard Procedure for Cost Analysis of Pollution Control Operations: Volume I, EPA 600/8-79-018a, June 1979.

small boilers and municipal waste combustors.^{2,3}. Based on this range of values, it is recommended that individual utilities use the contingency factor that would normally be used in-house in procurement or rate estimation procedures, and document the validity of the factor for the case in question. The factor recommended by OAQPS should be used as a default value when more appropriate information is not available."

Therefore a 10 percent contingency factor has been assumed for this project.

Based on the analysis in this section, the total capital investment for the SCR/oxidation catalyst control system is calculated as the sum of the total direct and indirect capital costs per OAQPS cost methods. The total capital investment for Unit 1 controlling  $NO_x$  and CO to 2.0 ppmvd and 1.8 ppmvd, respectively is estimated to be \$3,679,000.

The total capital investment for the SCONO_x control system is calculated as the sum of the total direct and indirect capital costs per OAQPS cost methods. The total capital investment for Unit 1 controlling NO_x and CO to 2.0 ppmvd and 1.8 ppmvd respectively is estimated to be \$10,555,000.

4.5.7.2 Operating Costs for SCR/Oxidation Catalyst Versus SCONO_x. Table 4-3 presents the annualized operating costs using a SCR/oxidation catalyst and SCONO_x system to achieve NO_x outlet emissions of 2.0 ppmvd and CO emissions of 1.8 ppmvd while firing natural gas for Unit 1. Annualized operating costs for the SCR/oxidation catalyst include catalyst replacement, energy impacts, operating personnel, maintenance, reagent and heat rate penalty. Throughout the life of the plant, catalyst elements for both the SCR and the oxidation catalyst will require periodic replacement. As the SCR catalyst becomes deactivated, ammonia slip emissions will increase. At the point ammonia slip approaches 5 ppmvd the catalyst must be replaced. The oxidation catalyst will degrade from normal operation that will be evident by an increase in CO emissions, thereby requiring replacement of the oxidation catalyst. Currently, SCR and oxidation catalyst manufacturers are willing to guarantee a catalyst life of three years of equivalent operating hours.

Ammonia consumption rates were based on a stoichiometric ratio of 1.05 for reacting NO_x. The heat rate penalty cost (lost power generation) item reflects the cost due to the SCR and oxidation catalyst backpressure losses. The additional backpressure will derate the combustion turbine resulting in lost electric sales revenue. The costs associated with these impacts are included in the annualized cost estimate.

²U.S. Environmental Protection Agency, <u>Industrial Boiler SO₂ Cost Report</u>, EPA 450/3-85-011, November 1984.

³U.S. Environmental Protection Agency, <u>Municipal Waste Combustors – Background Information for Proposed Standards: Control of NO_x Emissions, EPA 450/3-89-27d, August 1989.</u>

The use of either an SCR/oxidation catalyst system or a SCONO_x system increases the energy requirements of the project. The SCR system requires vaporizers and blowers to vaporize and dilute the ammonia reagent for injection. SCONO_x consumes power to open and close the catalyst dampers and to produce the regenerating gas. The maintenance costs will consist of routine system maintenance for each system. However, there is an additional annual maintenance cost for washing the SCONO_x/SCOSO_x catalyst. Therefore, the SCONO_x system will include the additional O&M cost for catalyst washing.

The indirect annual costs include capital recovery, overhead, administrative charges and insurance. The overhead annual cost is estimated to be 60 percent of the O&M costs. According to the OAQPS Cost Manual there are two types of overhead, payroll and plant. Payroll overhead expenses include workmen's compensation, social security, vacations, group insurance and other fringe benefits. Plant overhead is not tied into O&M of the control system, but is related to plant protection, control labs, employee amenities, plant lighting, parking areas, and landscaping. The OAQPS Cost Manual allows one to combine these overhead cost into one sum. The administrative cost covers sales, research and development, accounting, and other home office expenses. The insurance cost was based on 1 percent of the total capital investment for each system.

**4.5.7.3** Total Annualized Costs for SCR (2 ppmvd)/Oxidation Catalyst Versus SCONO_x. Total annualized costs for the SCR and oxidation catalyst control systems are calculated as the sum of operating costs plus the system capital recovery cost. The system capital recovery cost is the product of the system capital recovery factor (CRF) and the total capital investment (TCI). Table 4-3 shows the total annualized cost for a SCR/Oxidation Catalyst system for Unit 1 is estimated to be \$1,765,000, which is less than a third of the cost of a SCONOX system having a total annualized cost of \$5,355,000.

**4.5.7.4 Conclusions.** Based on the fact that the SCR/oxidation catalyst system is a lower capital cost system and has lower annualized costs than the SCONO_x system, the SCONO_x system will not be further evaluated as part of the BACT analysis. The remainder of the BACT analysis will concentrate on evaluating technologies for the control of each pollutant separately.

## 4.6 NO_x Only Energy, Environmental, and Economic Impacts Evaluation

The following section identifies economic impacts of the  $NO_x$  only BACT analysis. This section will not include a discussion of energy and environmental impacts, as they are the same as those discussed in the combined control BACT evaluation for  $NO_x$  and CO as listed in Section 4.5.

Table 4-3
NO_x/CO Combined Control Alternative Annualized Cost For Unit 1

	<b></b>	20010	SCR/OX	
	DLN	SCONOx	Cat	Remarks
Direct Annual Cost				Cost based on emissions in Table 4-1
Catalyst Replacement	N/A	1,414,000	660,000	Includes freight, installation, and 3-yr. capital recovery factor based on 3 yr. guaranteed catalyst life for SCR/OX cat and 5 year catalyst life for SCONOx.
Operation and Maintenance	N/A	38,000	22,000	See text for background information on this item
Maintenance Materials	N/A	23,000	11,000	
Reagent Feed	N/A	N/A	103,000	Assumes 1.05 stoichiometric ratio
Natural Gas Consumption	N/A	44,000	0	
Power Consumption	N/A	113,000	10,000	Includes injection blower and vaporization of ammonia
Lost Power Generation	N/A	2,187,000	417,000	Back pressure on combustion turbine. Includes seven days of lost power generation time for catalyst/system cleaning for SCONOX
Annual Distribution Check	N/A	56,000	28,000	Estimated as 0.5% of the total direct cost for SCONOX and 1% for SCR
Total Direct Annual Cost	N/A	3,875,000	1,252,000	
Indirect Annual Costs				
Overhead	N/A	23,000	13,000	60% of O&M Cost
Administrative Charges	N/A	307,000	102,000	2% of Installed Cost
Property Taxes	N/A	0	0	Not included
Insurance	N/A	154,000	51,000	1% of Installed Cost
Capital Recovery	N/A	996,000	347,000	Capital Recovery Excluding Catalyst
Total Indirect Annual Costs	N/A	1,480,000	513,000	
Total Annualized Cost	N/A	5,355,000	1,765,000	

#### 4.6.1 Economic Impacts for SCR

The control of NO_x emissions separate from CO emission control is possible through the application of a SCR to Unit 1 without additional CO emission controls. To determine the BACT levels for NO_x controls without the influence of the CO emission controls a separate economic analysis is required. An analysis of the economic impact of SCR as a separate control technology for NO_x emissions of 2.0 ppmvd is provided in this section. The BACT costs presented in this analysis are based on operating the combustion turbine, with duct firing, at 100 percent of base load for 8,760 hours per year on natural gas.

Unit 1 NO_x and CO BACT Analysis

#### 4.6.2 Economic Impacts for SCR (2.0 ppmvd NO_x) System

The use of an SCR has significant economic impacts to the TCEC Project. The application of SCR on Unit 1 must incorporate special design and operational/maintenance criteria, such as periodic catalyst replacements and increased associated plant outage costs. A detailed description of the economic impacts of SCR was provided previously in Subsection 4.5.7 and will not be repeated.

**4.6.2.1** Capital Costs for SCR (2.0 ppmvd NO_x). Table 4-4 summarizes the economic capital cost for implementing SCR on Unit 1. Based on the analysis in this section, the total installed capital costs for the SCR control system is calculated as the sum of the total direct and indirect capital costs per OAQPS cost methods. The total capital investment cost of SCR for Unit 1 controlling NO_x to 2.0 ppmvd is estimated to be \$2,996,000.

4.6.2.2 Total Annualized Costs for SCR (2.0 ppmvd NO_x). Total annualized costs for the SCR control systems are calculated as the sum of operating costs plus the system capital recovery cost. The system capital recovery cost is the product of the system capital recovery factor (CRF) and the total capital investment (TCI). Table 4-5 shows the total annualized cost for an SCR system is estimated to be \$1,306,000. This annualized cost for the Unit 1 SCR system results in a cost effectiveness of approximately \$3,546 per ton of NO_x removed.

#### 4.6.3 Conclusions

To summarize the information discussed in this section, SCR is considered a cost effective technology for control of emissions on Unit 1.

Table 4-4						
NO _x Emission Control Alternative Capital Cost for Unit 1						
	DLN	SCR	Remarks			
Direct Capital Cost			Cost based on emissions in Table 4-1.			
Catalyst	N/A	928,000	Estimated from NE Corporation			
Catalyst Reactor Housing	N/A	544,000				
Control/Instrumentation	N/A	140,000	Estimated; includes controls and monitoring equipment.			
Ammonia (Injection/Dilution/ Storage)	N/A	420,000				
Purchased Equipment Costs (PEC)	N/A	2,032,000				
Sales Tax		0	Not applicable to FMPA.			
Freight	N/A	203,000	10% of PEC			
Balance of Plant	N/A	610,000	30% of PEC. See text for background information on this item.			
Total Direct Cost (DC)	Base	2,845,000				
Indirect Capital Costs						
Contingency	N/A	285,000	10% of DC			
Engineering and Supervision	N/A	285,000	10% of DC			
Construction & Field Expense	N/A	142,000	5% of DC			
Construction Fee	N/A	285,000	10% of DC			
Start-up Assistance	N/A	57,000	2% of DC			
Performance Test	N/A	25,000	Assumed \$25,000			
Total Indirect Capital Costs (IC)	Base	1,079,000				
Installed Costs (DC + IC)		3,924,000	·			
Less SCR Catalyst Cost		928,000	Catalyst is viewed as an O&M value.			
Total Capital Investment, TCI	Base	2,996,000				

Table 4-5 NOx Emissions Control Annualized Cost for Unit 1						
DLN SCR Remarks						
Direct Annual Cost			Cost based on emissions in Table 4-1			
Catalyst Replacement	N/A	427,000	Includes freight, installation, and 3-yr capital recovery factor based on 3 yr. guaranteed catalyst life			
Operation and Maintenance	N/A	22,000	See text for background information			
Maintenance Materials	N/A	11,000	See text for background information			
Reagent Feed	N/A	103,000	Assumes 1.05 stoichiometric ratio			
Power Consumption	N/A	10,000	Includes injection blowers and vaporization of ammonia			
Lost Power Generation	N/A	292,000	Back pressure on combustion turbine			
Annual Distribution Check	N/A	28,000	Estimated as 1 % of the total direct cost			
Total Direct Annual Cost	N/A	893,000				
Indirect Annual Costs	N/A					
Overhead	N/A	13,000	60% of Operation and Maintenance cost			
Administrative Charges	N/A	78,000	2% of Installed Costs			
Property Taxes	N/A	0	Not included			
Insurance	N/A	39,000	1% of Installed Costs			
Capital Recovery	N/A	283,000	Capital recovery excluding catalyst			
Total Indirect Annual Cost	N/A	413,000				
Total Annualized Cost	N/A	1,306,000				
NO _x Annual Emissions, tpy	440.6	72.3	Emission taken from Table 4-1			
NO _x Emissions Reduction, tpy	N/A	368.3	Emissions calculated in Table 4-1			
NO _x Total Cost Effectiveness, \$/ton	N/A	3,546	Total Analyzed Cost/Emissions Reduction			

## 4.7 CO Only Energy, Environmental, and Economic Impacts Evaluation

The following section identifies economic impacts of the CO only BACT analysis. This section will not include discussion of energy and environmental impacts, as they are the same as listed in the combined control BACT evaluation for NO_x and CO as listed in Section 4.5.

#### 4.7.1 Economic Impacts for Oxidation Catalyst

The use of an oxidation catalyst has significant economic impacts to the TCEC Project. An analysis of the economic impact is provided in this section. The BACT costs presented in this analysis are based on operating each combustion turbine, with duct firing, at 100 percent of base load for 8,760 hours per year on natural gas. The oxidation catalyst is used to reduce CO emissions.

#### 4.7.2 Capital Cost for Oxidation Catalyst

Table 4-6 presents the capital costs for installing an oxidation catalyst on the units during natural gas firing to achieve a CO outlet emission level of 1.8. The capital costs for the systems includes the oxidation catalyst, oxidation catalyst reactor housing, controls and instrumentation, sales taxes and freight, and were based on budgetary quotations from equipment manufacturers and other engineering estimates. The direct installation costs included the balance of plant items such as foundations, insulation and lagging, and painting, and were calculated as percentages of the total purchased equipment costs (PEC). The total capital investment was calculated as the summation of the total direct cost (DC) and total indirect costs (IC) per OAQPS cost methods. The indirect capital costs for the SCR/Oxidation Catalyst systems are percentages of the total direct cost (DC) and are site specific. The three percent contingency value suggested in the OAQPS Cost Control Manual is judged to be inaccurate as compared to actual values typically used in the construction field for this level of estimating, as discussed in Section 4.5.7.1.

Total capital costs for the oxidation catalyst control system to reduce CO is calculated as the sum of the direct and indirect installed costs. The total capital investment per unit for an oxidation catalyst system to reduce CO emissions from Unit 1 is estimated to be \$683,000.

#### 4.7.3 Operating Costs for Oxidation Catalyst

Table 4-7 presents the annualized operating costs and emission rates using an oxidation catalyst to achieve a 77.5 percent reduction in CO emissions while firing natural gas on Unit 1. Annualized operating costs for the system includes catalyst

Table 4-6
CO Reduction System Capital Cost For Unit 1

	Good Combustion Controls/DLN	Oxidation Catalyst	Remarks
Direct Capital Cost			Cost based on emissions in Tables 4-1.
Oxidation Catalyst	N/A	508,000	Estimated from NE Corporation
Catalyst Reactor Housing	N/A	60,000	
Control/Instrumentation	N/A	40,000	Estimated; includes controls and monitoring equipment.
Purchased Equipment Costs (PEC)	N/A	608,000	
Sales Tax	N/A	0	Not applicable to FMPA
Freight	N/A	61,000	10% of PEC
Balance of Plant	N/A	182,000	30% of PEC. See text for background information on this item.
Total Direct Cost (DC)	Base	851,000	·
Indirect Capital Costs	N/A		
Contingency	N/A	85,000	10% of DC
Engineering and Supervision	N/A	85,000	10% of DC
Construction & Field Expense	N/A	43,000	5% of DC
Construction Fee	N/A	85,000	10% of DC
Start-up Assistance	N/A	17,000	2% of DC
Performance Test	N/A	25,000	Assumed value of \$25,000
Total Indirect Capital Costs (IC)	Base	340,000	
Installed Costs (DC +IC)		1,191,000	
Less Catalyst	N/A	508,000	Catalyst is viewed as an O&M Value.
Total Capital Investment, TCI	Base	683,000	

CO	Table 4-7 CO Control Annualized Cost For Unit 1											
	Good Combustion Controls/DLN	Oxidation Catalyst	Remarks									
Direct Annual Cost			Cost based on emissions in Tables 4-1.									
Catalyst Replacement	N/A	234,000	Includes freight, installation, and 3-yr. capital recovery factor based on 3 yr. guaranteed catalyst life.									
Operation and Maintenance	N/A	0	Not applicable for Oxidation Catalyst									
Lost Power Generation	, ,	125,000	Back pressure on combustion turbine									
Total Direct Annual Cost	N/A	359,000										
Indirect Annual Costs												
Overhead	N/A	0	Not Applicable because of zero O&M									
Administrative Charges	N/A	24,000	2% of Installed Costs									
Property Taxes	N/A	0	Not included									
Insurance	N/A	12,000	1% of Installed Costs									
Capital Recovery	N/A	64,000	Capital recovery excluding catalyst.									
Total Indirect Annual Costs	N/A	100,000										
Total Annualized Cost	Base	459,000										
CO Annual Emissions, tpy	173.9	39.1	Emissions taken from Table 4-1.									
CO Emissions Reduction, tpy	N/A	134.8	Emissions taken from Table 4-1.									
CO Total Cost Effectiveness, \$/ton	N/A	3,405	Total Annualized Cost/Emissions Reduction									

replacement and lost power generation. Throughout the life of the plant, catalyst elements will require periodic replacement. Currently, catalyst manufacturers are willing to guarantee an oxidation catalyst life of three years of equivalent operating hours for an oxidation catalyst.

### 4.7.4 Total Annualized Costs for Oxidation Catalyst

Total annualized costs for the oxidation control system is calculated as the sum of operating costs plus the system capital recovery cost. The system capital recovery cost is the product of the system capital recovery factor (CRF) and the total installed costs. The total annualized cost for a 1.8 ppmvd CO oxidation catalyst system for Unit 1 is estimated to be \$459,000. This annualized cost for Unit 1 results in a cost effectiveness of approximately \$3,405 per ton of CO removed.

#### 4.7.5 Conclusions

Based on the high cost effectiveness value for the CO catalyst it is determined that add-on controls to further reduce CO emissions are unwarranted given the low CO emission characteristics of Unit 1 firing natural gas as the primary fuel. BACT for CO emissions control for Combustion Turbine Unit 1 is Dry Low NO_x burners with good combustion control.

138859 4-25

### 5.0 Unit 1 PM/PM₁₀ BACT Analysis

The objective of this analysis was to determine BACT for PM/PM₁₀ emissions from Unit 1. This includes the combustion turbine and supplemental firing from duct burners in the HRSG as a total unit.

PM/PM₁₀ emissions from the combustion turbine are a result of incomplete combustion and trace particulate parameters in the fuel. The emissions of particulate matter from Unit 1 will be controlled by ensuring as complete combustion of the fuel as possible. The NSPS for combustion turbines do not establish a particulate emission limit. Natural gas contains only trace quantities of non-combustible material.

The manufacturer's standard operating procedures include filtering the turbine inlet air and combustion controls. The BACT/LAER Clearinghouse documents do not list any post-combustion particulate matter control technologies being used on combustion turbines. Consistent with the previous determinations as referenced by the State of Florida, such as the FPL Turkey Point, FPL Martin, FPL Manatee, FPL Fort Myers, Santa Rosa and the City of Tallahassee projects, the use of combustion controls and natural gas (low sulfur fuel) is considered BACT for particulate matter and is proposed for Unit 1. Ultra-low sulfur fuel oil will only be used as a backup fuel. Limited operation while firing ultra-low sulfur fuel oil in the combustion turbine is considered BACT

138859 5-1

### 6.0 Unit 1 SO₂ BACT Analysis

The objective of this analysis was to determine BACT for SO₂ emissions from Unit 1. The SO₂ emissions are based on operating the combustion turbine with duct firing at 100 percent of base load for a total of 8,760 hours while firing natural gas.

Typically, natural gas has only trace amounts of sulfur that is used as an odorant. The selection of natural gas fuel provides inherently low SO₂ emissions.

Emissions of SO₂ can be controlled by limiting sulfur content in the fuel, limiting fuel oil usage, or by a post-combustion flue gas desulfurization (FGD) system. The fuel for this project is natural gas with a maximum expected sulfur content of 2.0 grains per 100 standard cubic feet. In addition, when the unit is firing fuel oil, the unit will fire ultra-low sulfur fuel oil which has a sulfur content of 0.0015 percent sulfur by weight.

To date, no supplemental SO₂ emission controls, such as flue gas desulfurization system (FGD) systems have been imposed on combined cycle combustion turbines. Such a system would be both technically and economically prohibitive.

Therefore, BACT for Unit 1 is the use of natural gas or ultra-low sulfur fuel oil with less than 0.0015 percent sulfur by weight. Basis of this determination is firing natural gas up to a maximum of 8,760 hours per year as the primary fuel and firing ultra-low sulfur fuel oil a maximum of 500 hours per calendar year as a backup fuel.

138859 6-1

### 7.0 Unit 1 H₂SO₄ BACT Analysis

The objective of this analysis was to determine BACT for sulfuric acid mist (H₂SO₄) emissions from Unit 1. The H₂SO₄ emissions are based on operating the combustion turbine with duct firing at 100 percent of base load for a total of 8,760 hours while firing natural gas.

Emissions of H₂SO₄ can be controlled by limiting sulfur content in the fuel. The natural gas (primary fuel) and ultra-low sulfur fuel oil to be utilized for Unit 1 will contain less than 2 grains per 100 standard cubic feet and 0.0015 percent sulfur by weight, respectively. The selection of low sulfur fuel (both natural gas and ultra-low sulfur fuel oil) provides inherently low SO₂ emissions, thus controlling the formation of sulfuric acid mist. In addition, no supplemental SO₃ emission controls, such as FGD systems or H₂SO₄ abatement systems, have been imposed on natural gas fired or low sulfur fuel oil fired combustion turbines by regulatory agencies.

Therefore, BACT for Unit 1 is the use of good combustion controls while firing natural gas or ultra-low sulfur fuel oil with less than 0.0015 percent sulfur by weight. The basis of this determination is firing natural gas up to a maximum of 8,760 hours as the primary fuel and firing ultra-low sulfur fuel oil a maximum of 500 hours as a backup fuel per calendar year.

138859 7-1

### 8.0 Conclusions

The following is a summary of the proposed BACT determinations and associated emission rates for Unit 1 to be installed at the Treasure Coast Energy Center for FMPA. Unit 1 will fire natural gas as the primary fuel and ultra-low sulfur fuel oil as the backup fuel. Emissions and conclusions for the BACT analysis are based on Unit 1 operating a maximum of 8,760 natural gas hours per year at an average ambient temperature of 73° F. Firing on ultra-low sulfur fuel oil is based upon a maximum 500 hours per year of operation.

- Nitrogen oxides (NO_x) emissions--BACT was determined to be the use of selective catalytic reduction to achieve 2 ppmvd at 15 percent O₂ while firing natural gas and 8 ppmvd at 15 percent O₂ while firing ultra-low sulfur fuel oil in accordance with the defined operating hours for each fuel.
- <u>Carbon monoxide (CO)</u> emissions--BACT was determined to be the use of good combustion controls while firing natural gas or ultra-low sulfur fuel oil with less than 0.0015 percent sulfur by weight in accordance with the defined operating hours for each fuel.
- Particulate (PM/PM₁₀) emissions--BACT was determined to be the use of good combustion controls and firing natural gas or ultra-low sulfur fuel oil with less than 0.0015 percent sulfur by weight in accordance with defined operating hours for each fuel.
- <u>Volatile Organic Compounds (VOC) emissions</u>--The emissions of VOCs will be less than the major source PSD threshold level. Therefore a BACT analysis for VOCs is not required for Unit 1.
- <u>Sulfur dioxide (SO₂) emissions</u>--BACT was determined to be the use of natural gas or ultra-low sulfur fuel oil with less than 0.0015 percent sulfur by weight in accordance with the defined operating hours for each fuel.
- <u>Sulfur acid mist (H₂SO₄) emissions</u>—BACT was determined to be the use of good combustion controls while firing natural gas or ultra-low sulfur fuel oil with less than 0.0015 percent sulfur by weight in accordance with the defined operating hours for each fuel.

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### 9.0 Unit 1 Auxiliary Boiler

Unit 1 will utilize a 7.2 MBtu/h package boiler for supplemental steam supply for startup operations of the Unit 1 combined cycle system. The auxiliary boiler will fire only natural gas which results in minimal emissions. Due to the size of the Unit 1 auxiliary boiler, post combustion emissions controls for NO_x such as SCR or SNCR, emissions controls for SO₂ such as flue gas desulfurization systems, or emission controls for CO such as oxidation catalyst have not been employed or required. Therefore, the proposed BACT for the Unit 1 Auxiliary Boiler is good combustion controls while firing natural gas.

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### 10.0 Unit 1 Safe Shutdown Diesel Generator

A review of the RBLC indicates that this type of emergency equipment has not been required to install additional NO_X controls because of intermittent operation. The remaining pollutants are controlled by good combustion controls. Due to the size of the safe shutdown diesel generator and the fact that this is emergency equipment, post combustion emissions controls for NO_X such as SCR or SNCR, emissions controls for SO₂ such as flue gas desulfurization systems, or emission controls for CO such as oxidation catalyst are not considered BACT. Therefore, the proposed BACT for the safe shutdown diesel generator is good combustion controls while firing ultra low sulfur distillate oil. The proposed BACT has no adverse environmental or energy impacts.

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### 11.0 Unit 1 Mechanical Draft Cooling Tower

Heat rejection needs (i.e. cooling) will be accomplished by the use of a mechanical draft cooling tower with multiple cells. The mechanical draft cooling tower will be an induced draft cooling tower system in which the cooling fans are located downstream of the tower fill.

The only emissions expected from the mechanical draft cooling tower is PM and PM₁₀ in the form of cooling tower drift. Cooling tower drift is dissolved solids contained in droplets of the cooling water that escape past the drift eliminators. The design of the cooling towers and drift eliminators will be to maintain a drift rate less than 0.0005 percent of the circulating water flow rate. The drift rate expected, based on the design of the Unit 1 Mechanical Draft Cooling Tower, is consistent with recently permitted combined cycle combustion turbine plants such as FPL Turkey Point and is the proposed BACT for Unit 1. The proposed BACT has no adverse environmental or energy impacts.

138859

### 12.0 Unit 1 Emergency Diesel Engine Fire Pump

The uncontrolled emissions for the emergency diesel fire pump is based on engine design and is proposed as BACT. A review of the RBLC indicates that this type of equipment has not been required to install any additional emissions controls because the fire pump will operate only during tests to ensure operability and during times of emergency. The typical emissions from the emergency diesel engine fire pump are controlled by good combustion controls. The proposed BACT has no adverse environmental or energy impacts.

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## Appendix A NO_x/CO Control Technology Review for Unit 1

Table A-1
NO _x BACT Clearinghouse Review List

Facility	State	Permit Date	Process	Output	Emission limit, ppmvd @ 15% O ₂	Control Technology
FPL Bellingham	MA	AUG-99	Turbine, Combined Cycle, Natural Gas	~545 MW	1.5 (1 hour - 90% of time) 1.5-2.0 (10% of time)	SCR
Federal Cold Storage Cogeneration	CA	DEC-96	GE LM2500-M-2	222 MBtu/h	2.0	Water Injection, SCONOx
Sithe Mystic	MA	JAN-01	Turbine, Combined Cycle, Natural Gas	~775 MW	2.0	SCR
Duke Energy Arlington Valley	AZ	NOV-03	Turbine, Combined Cycle, Natural Gas	600 MW	2.0	SCR
Duke Morro	CA	NOV-00	Turbine, Combined Cycle, Natural Gas	1200	2	SCR
PDC El Paso Milford LLC	CT	APR-99	ABB GT-24 w/chillers (x 2)	~180 MW	2.0	SCR
FPL Turkey Point	FL	FEB-05	Combined Cycle	1,150 MW	2.0	SCR
ANP Bellingham Energy Company	MA	AUG-99	Combined Cycle	Combined Cycle 580 MW 2.0		SCR
Reliant Energy Hope	RI	MAY-00	Combined Cycle	bined Cycle 4,624 2.0 MBtu/h		SCR
Goldendale Energy Inc.	WA	FEB-01	Combined Cycle	248.7 MW	2.0	SCR
Calpine OEC	PA	NOV-00	Combined Cycle	~550 MW	2.0 NG (3 hour) 2.5 NG (1 hour)	SCR
Cogen Tech, NJ	NJ	DEC-99	Combined Cycle	181MW	2.5 (1 hour)	SCR
Sutter Power Plant	CA	APR-99	SW 501F	170 MW	2.5	Dry low NOx, SCR
El Paso Belle Glade Energy Center	FL	SEP-01	Combined Cycle	600 MW	2.5	Dry low NOx, SCR
La Paloma Generating Co.LLC	CA	MAY-99	ABB Model GT-24	262 MW	2.5	Dry-low NOx, SCR
El Paso Manatee	FL	APR-02	Combined Cycle	600	2.5 (24 hour) NG	Dry-low NOx, SCR
FPL Manatee	FL	APR-03	Combined Cycle	1150	2.5 (24 hour) NG	Dry-low NOx, SCR
FPL Martin	FL	APR-03	Combined Cycle	1150	2.5 (24 hour) NG 12-FO	Dry-low NOx, SCR

### Table A-1 (Continued) NO_x BACT Clearinghouse Review List

Facility	State	Permit Date	Process	Output	Emission limit, ppmvd @ 15% O ₂	Control Technology
PGN Hines III	FL	SEP-03	Combined Cycle	530	2.5 (24 hour) NG 10-FO	Dry-low NOx, SCR
Turlock Irrigation District	CA	AUG-94	GE LM5000	417 MBtu/h	3.0	SCR, Steam Injection
Sacramento Power Authority (Campbell Soup)	CA	AUG-94	Siemens V84.2	1,257 MBtu/h	3.0	Water injection, SCR
Choctow County, LLC	MS	NOV-03	Turbine, Natural Gas Fired	230 MW each Turbine	3.5	SCR
Casco Ray Energy Co.	ME	JUL-98	Turbine, Combined Cycle, Natural Gas	170 MW	3.5	SCR
Granite Road Limited	CA	MAY-91	Turbine, Gas	460.9 MBtu/h	3.5	SCR, Steam Injection
Enron/Ft. Pierce	FL	AUG-01	Turbine, Combined Cycle, Natural Gas	~250 MW	3.5 NG (3 hour) 10 FO	SCR

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Table A-2
CO BACT Clearinghouse Review List

Facility	State	Permit Date	Process	Output, MW	Emission limit ppmvd @ 15% O ₂ or as indicated	Control Technology
Newark Bay Cogeneration Partnership, L.P.	NJ	JUN-93	Turbines, Combustion Natural Gas Fired	137	1.8	Oxidation Catalyst
Longview Energy Development	WA	AUG-01	Combine Cycle	290	2.0	Oxidation Catalyst
FPL Bellingham	MA	AUG-99	Turbine, Combined Cycle, Natural Gas	~545 MW	2.0	Oxidation Catalyst
Sithe Mystic	CA	JAN-01	Turbine, Combined Cycle, Natural Gas	~775 MW	2.0	Oxidation Catalyst
Cogen Tech, NJ	NJ	DEC-99	Cogeneration	181MW	2.0 (1 hour)	Oxidation Catalyst
Duke Morro	CA	NOV-03	Turbine, Combined Cycle, Natural Gas	1200	2	Oxidation Catalyst
El Paso Manatee	FL	APR-03	Combined Cycle	2.5 (3 hour) NG 4 (3 hour, PA) NG	Oxidation Catalyst	
Saranac Energy Company	NY	JUL-92	Turbines, Combustion Natural Gas Fired	1123	3	Oxidation Catalyst
Blue Mountain Power, L.P	PA	JUL-96	Combustion Turbine with Heat Recovery Boiler	153	3.1	Oxidation Catalyst
Enron/Ft. Pierce	FL	AUG-01	Turbine, Combined Cycle, Natural Gas	~250 MW	3.5 NG (3 hour) 10 Low Load 8-FO	Oxidation Catalyst
Sutter Power Plant	CA	APR-99	Turbine, SW 501F	170	4	Oxidation Catalyst
Brooklyn Navy Yard Cogeneration Partners, L.P	NY	JUN-95	Turbine, Natural Gas Fired	240	4	No Control
FPL Turkey Point	FL	FEB-05	Combined Cycle	1,150 MW	4.1 NG (DB Off) 7.6 NG (DB On) 14.1 NG (DB +PA) 8.0 FO	Good Combustion Control

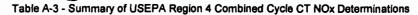
## Table A-2 (Continued) CO BACT Clearinghouse Review List

Facility	State	Permit Date	Process	Output, MW	Emission limit ppmvd @ 15% O ₂ or as indicated	Control Technology
Crockett Cogeneration (C&H Sugar)	CA	OCT-93	GE PG7221 (FA)	240	5.9	Good Combustion Control
FPL Manatee	FL	APR-03	Combined Cycle	1150	8 -NG(DB off) 10 -NG(DB, PA)	Good Combustion Control
FPL Martin	FL	APR-03	Combined Cycle	1150	7.4 -NG (New, Clean) 8 -NG(DB off) 10 -NG(DB, PA)	Good Combustion Control
Calpine OEC	PA	NOV-00	Combined Cycle	~550 MW	10 NG(1 hour)	Good Combustion Control
PGN Hines III	FL	SEP-03	Combined Cycle	530	10 NG(1 hour) 20-FO	Good Combustion Control
Milford Power	СТ	APR-99	ABB GT-24	~550 MW	13-52 lb/h	Oxidation Catalyst
Mobile Energy, LLC - Hog Bayou	AL	JAN-99	GE 7FA	170	0.04 lb/MBtu	Good Combustion Control
Alabama Power, Plant Barry	AL .	AUG-98	GE 7FA	170	0.057 lb/MBtu	Good Combustion Control
Alabama Power, Plant Barry	AL	AUG-99	GE 7FA	170	0.06 lb/MBtu	Good Combustion Control
Alabama Power Theodore Cogeneration Facility	AL	MAR-99	GE 7FA	170	0.086 lb/MBtu	No Control

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State	Facility	# of New MW	Final Permit	# of CTs	# of DB	Turbine Model	Fuel	Mode	Hours	NOx Limit	Control	Avg. Time	Comments
Region 4													
AL	Alabama Power - Olin Cogeneration	137	12/01/1997	1	1	GE 7EA (80 MW)	NG	СС	8,760	15 ppm	DLN		Power Augmentation
AL	Alabama Power - GE Plastics Cogeneration	100	05/01/1998	1	1	GE 7EA (80 MW)	NG	СС	8,760	9 ppm; 0.20 lb/MMBtu (DB)	DLN		
AL	Alabama Power, Plant Barry	800	08/01/1998	3	3	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm / 0.013 lb/MMBtu	DLN/SCR		
AL	Alabama Power, Plant Barry	200	08/01/1999	1	1	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm / 0.013 lb/MMBtu	DLN/SCR		
AL	Mobile Energy, LLC - Hog Bayou	200	1-99	1	1	GE 7FA (168 MW)	NG; FO	СС	8,760; 675 FO	3.5 ppm NG; 41 ppm w/ FO	DLN/SCR; WI		
AL	Alabama Power - Theodore Cogeneration Facility	210	3-99	1	1	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm/ 0.013 lb/MMBtu	DLN/SCR		
AL	Tenaska Alabama Partners	846	11-99	3	3	GE 7FA (170 MW)	NG; FO	СС	8,760; 720 FO	3.95 ppm NG; 11.3 ppm FO	DLN/SCR; WI/SCR		
AL	Georgia Power - Goat Rock	•	4-00	8	8	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm/ 0.013 lb/MMBtu	DLN/SCR		
AL	Georgia Power - Goat Rock (revision of above PSD application)	2,460	4-01	8	8	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm/ 0.013 lb/MMBtu	DLN/SCR		
AL	Alabama Electric Cooperative - Gantt Plant	500	3-00	2	2	SW 501F (166 MW)	NG	СС	8,760	3.5 ppm / 0.013 lb/MMBtu	DLN/SCR		
ΑĹ	South Eastern Energy Corp.	1,500	1-01	6	6 if CC	GE 7FA or SW 501F	NG	SC or CC	8,760	9 or 25 or 3.5 ppm	DLN if SC/SCR if CC		For NOx and CO: SC w/GE or SC w/SW501F or CC (either)
AL	Calpine Solutia - Decatur	700	6-00	3	3	SW501F (180 MW)	NG	СС	8,760	3.5 ppm/ 0.013 lb/MMBtu	SCR		
AL	Calpine BP Amoco	700	6-00	3	3	SW501F (180 MW)	NG	СС	8,760	3.5 ppm/ 0.013 ib/MMBtu	SCR		
AL	Tenaska Alabama II Generating Station	900	2-01	3	3	GE 7FA or Mitsubishi M501F	NG; FO	СС	8,760; 720 FO	0.013/0.048 lb/mmbtu NG/FO - GE; 0.013/0.046 lb/mmbtu NG/FO - Mit	SCR/WI		
AL	Hillabee Energy Center	700	1-01	2	2	SW501G (229 MW)	NG	СС	8,760	3.5 ppm	DLN/SCR		PA = Power Augmentation, DB= Duct Burning
AL	Duke Energy - Alexander City	1,260	2-01	10	2	GE 7FA & 7EA	NG	CC & SC	8,760 CC; 2,500 SC	3.5 ppm (0.013 lb/mmBtu) CC; 9/12 ppm (0.033 lb/mmBtu) SC	SCR - CC, DLN-SC	an/1- hr	8 SC units and 2 CC units
AL	GenPower - Kelly, LLC	1,260	1-01	4	4	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm	SCR		
AL	Blount County Energy	800	1-01	3	3	"F" Class (170 MW)	NG	СС	8,760	0.013 lb/mmBtu (30.7 lb/hr)	SCR	3-hr	
AL	Alabama Power - Autaugaville	1,260	1-01	4	4	"F" Class (170 MW)	NG	СС	8,760	3.5 ppm (0.013 lb/mmBtu)	SCR		
AL	Tenaska Alabama IV Partners	1,840	10/09/2001	6	6	Mit 501F (170 MW)	NG; FO	СС	8,760; 720 FO	3.5 ppm NG; 12 ppm FO	SCR		SCONOx - \$6,145/ton NOX; CatOx- \$1,506/ton CO
AL	Duke Energy Autauga, LLC	630	10/29/2001	2	2	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm	SCR		SCONOx - \$18760/ton NOX; CatOx- \$5,006/ton CO





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AL	Duke Energy Dale, LLC	630	12/17/2001	2	2	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm (0.013 lb/mmbtu)	SCR		SCONOx - \$18,403/ton NOX; CatOx- \$2,634/ton CO+VOC
AL	Barton Shoals Energy, LLC	1,200	07/15/2002	4	4	GE 7FA (170 MW)	NG	СС	8,760	2.5 ppm (0.0092 lb/mmbtu)	SCR		EPA did not received application until 5/24/02
FL	City of Lakeland, McIntosh Power Plant	250	7-10-98	1	0	SW 501G (230 MW)	NG; FO	SC (later CC)	7,008; 250 FO	25 ppm until 5/2002, 9 ppm after, 7.5 ppm if CC. NG; 42 ppm or 15 ppm FO	DLN or SCR; WI or SCR		Power Augmentation
FL	Santa Rosa Energy Center, Sterling Fibers Mfg. Facility	241	12-4-98	1	1	GE 7FA (167 MW)	NG	СС	8,760	9 ppm, 9.8 ppm w/ DB	DLN		If a different CT is used, SCR may be required to meet 6 ppm NOx)
FL	Kissimmee Utility Authority, Cane Island Power Park -Unit 3	250	draft permit	1	0	GE 7FA (167 MW)	NG; FO	СС	8,760; 720 FO	3.5 ppm NG; 15 ppm FO	SCR		
FL	Duke Energy - New Smyrna Beach	500	draft permit	2	0	GE 7FA (165 MW)	NG	СС	8,760	9 ppm or 6 ppm	DLN or SCR		
FL	City of Tallahassee - Purdom	250	5-98	1	0	GE 7FA (160 MW)	NG; FO	СС	8,760	12 ppm NG; 42 ppm FO	DLN; WI	30- day	
FL	Gulf Power - Smith Station	340	7-00	2	2	GE 7FA (170 MW)	NG	СС	8,760	82.9 lb/hr w/DB, 113.2 lb/hr w/ DB & SA	DLN	30- day	Netting out of PSD for NOx and CO; SA = steam augmentation
FL	Florida Power & Light - Sanford	2,200	9-99	8	0	GE 7FA (170 MW)	NG, FO	СС	8,760; 500 FO	9 ppm NG; 42 ppm FO	DLN; WI		Repowering, 4 units FO
FL	Gainesville Regional Utilities, Kelly Generating Station	133	2-00	1	0	GE 7EA (83 MW)	NG; FO	СС	8,760; 1,000 FO	9 ppm NG; 42 ppm FO	DLN; WI		Netting out of PSD review for NOx
FL	Calpine Osprey Energy Center	527	07/05/2001	2	2	501FD (170 MW)	NG	СС	8,760	3.5 ppm	DLN/SCR	24-hr Block	2,800 hr/yr - Power Aug. mode
FL	Hines Energy ( FPC)	530	06/07/2001	2	0	5W 501FD (170 MW)	NG; FO	CC	8,760; 1,000 FO	3.5 ppm NG; 12 ppm FO	SCR; WI	24-hr Block	SCONOx - \$16,712/ton NOx.; CatOx - \$2,130/ton CO
FL	CPV - Gulfcoast	250	2-01	1	0	GE 7FA (170 MW)	NG; FO	СС	8,760; 720 FO	3.5 ppm NG; 10 ppm FO	SCR		SCONOx - no cost eval.; CatOx - \$4,350/ton CO
FL	TECO Gannon/Bayside	1,728	3-01	7	0	GE 7FA (170 MW)	NG; FO	СС	8,760; 876 FO	3.5 ppm NG; 16.4 ppm FO	SCR		Repowering project: netting out of NOx, CO, PM10 and SO2 review (subject to VOC revelw)
FL	South Pond Energy Park	600	draft permit	3	0	GE 7FA (170 MW)	NG; FO	sc/cc	3,390/8, 760; 720 FO	9 ppm /2.5 ppm NG; 36/10 ppm FO	DLN/SCR; WI	3-hr	2 SC CT and 1 CC CT also capable of operating in SC mode.
FL	North Pond Energy Park	430	applic. under review	2	0	GE 7FA (170 MW)	NG; FO	SC/CC	3,390/8, 760; 720 FO	10 ppm (9 initial)/3.5 ppm NG; 42/15 ppm FO	DLN/SCR; WI	3-hr	1 SC CT and 1 CC CT also capable of operating in SC mode.
FL	Calpine Blue Heron Energy Center	1,080	draft permit	4	4	SW 501F (170 MW)	NG	СС	6,760	3.5 ppm	DLN/SCR		base/duct burner/power aug./60-70% load; SCONOx - \$9,982/ton NOx; CatOx - \$1,553/ton CO
FL	Jacksonville Electric Authority - Brandy Branch (revision)	200	03/29/2002	0	2	GE 7FA (170 MW)	NG; FO	СС	8760; 288 FO	3.5 ppm NG; 15 ppm FO	SCR	3-hr	Conversion of 2 SC units to 2 CC units
FL	CPV - Atlantic Power	250	05/03/2001	1	0	GE 7FA (170 MW)	NG; FO	2	8,760; 720 FO	3.5 ppm NG; 10 ppm FO	SCR		PA = Power Augmentation

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	Orlando Utilities - Curtis H			····		CE 75A	NO:		0.760	2 5 nom NO: 40			
FL	Stanton Energy Center	633	09/26/2001	2	2	GE 7FA (170 MW)	NG; FO	СС	8,760; 1000 FO	3.5 ppm NG; 10 ppm FO	SCR		
FL	Broward Energy Center	775	05/15/2002	4	0	GE 7FA (175 MW)	NG	cc/sc	000	2.5 ppm/9 ppm	SCR/DLN	24-hr	1 CC w/unfired HRSG & 3 SC; PA = Power Augmentation
FL	Belle Glade Energy Center	600	01/28/2002	3	0	GE 7FA (175 MW)	NG	CC/SC	8,760/5, 000	2.5 ppm/9 ppm	SCR/DLN	24-hr	1 CC w/unfired HRSG & 2 SC; PA = Power Augmentation
FL	Manatee Energy Center	600	01/17/2002	3	0	GE 7FA (175 MW)	NG	cc/sc	8,760/5, 000	2.5 ppm/9 ppm	SCR/DLN	24-hr	1 CC w/unfired HRSG & 2 SC; PA = Power Augmentation
FL	CPV Pierce Power Generation Facility	250	08/17/2001	1	0	GE 7FA (170 MW)	NG; FO	СС	8,760; 720 FO	2.5 ppm NG; 10 ppm FO	SCR	24-hr	PA limited to 2,000 hr/yr
FL	Fort Pierce Repowering Project	180	08/15/2001	1	1	SW 501F (180 MW)	NG; FO	cc/sc	8,760; 1,000 FO/2,00 0; 500 FO	3.5 ppm NG; 12 ppm FO/25 ppm NG; 42 ppm FO	SCR/DLN; WI		CT will operate in both CC and SC modes
FL	TECO Bayside Power Station (repowering)	1,032	01/09/2002	4	0	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm	SCR	24-hr	Repowering Project: Netting out of PSD for NOx, SO2, lead and SAM (subject for PM10, VOC and CO)
FL	CPV Cana Power Generation Facility	245	01/17/2002	1	1	GE 7FA (170 MW)	NG; FO	СС	8,760; 720 FO	2.5 ppm NG; 10 ppm FO	SCR	24-hr	PA limited to 2,000 hr/yr; CO w/FO: 90-100%/76-89%/50- 75% load
FL	FPL Martin	1,150	04/16/2003	4	0	GE 7FA (170 MW)	NG; FO	cc/sc	8,760; 5000 FO/1,00 0; 500 FO	2.5 ppm NG; 10 ppm FO/9-15 ppm NG; 42 ppm FO	SCR/DLN; WI	24-hr	PA = Power Augmentation
FL	FPL Manatee	1,150	04/15/2003	4	4	GE 7FA (170 MW)	NG	cc/sc	8,760/1, 000	2.5 ppm CC/9-15 ppm SC	SCR/DLN	24-hr	PA = Power Augmentation
FL	FPC - Hines Energy Complex	530	09/19/2003	2	0	5W 501FD (170 MW)	NG; FO	СС	8,760; 720 FO	2.5 ppm NG/10 ppm FO	SCR	24-hr	SCONOx - \$8,597/ton NOx;
FL	FPL Turkey Point	1,150	draft permit	4	4	GE 7FA (170 MW)	NG; FO	СС	8,760; 500 FO	2.0 ppm NG/8.0 ppm FO	SCR	24-hr	SCR (3.5ppm) = \$3,744/ton NOx; SCR (2.5 ppm) = \$3,753/ton NOx
GA	Georgia Power - Wansley	2,280	07/28/2000	8	8	GE 7FA (170 MW)	NG	CC	8,760	3.5 ppm / 0.013 lb/MMBtu	DLN/SCR	30 day	
GA	(Oglethorpe Power)  Duke Energy Murray, LLC	1,240	2-01	4	4	GE 7FA (170 MW)	NG	СС	8,760	3.0 ppm*	DLN/SCR	usy	NOx and CO BACT limits were lowered from 3.5 ppm and 22 ppm after the permit was issued in response to a settlement with an Environmental Group
GA	Duke Energy Buffalo Creek, LLC	620	applic. under review	2	2	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm	DLN/SCR		SCONOx - \$19,948/ton NOx; CatOx - \$2,469/ton CO
GA	Augusta Energy LLC	750	09/28/2001	3	3	GE 7FA (170 MW)	NG; FO	СС	8,760; 1,000 FO	3.5 ppm NG; 42 ppm FO	SCR; WI		SCONOx - \$17,490/ton NOx; CatOx - \$1,828/ton CO

Table	A-3 - Summary of USEPA Region	4 Combined	d Cycle CT NO:	x Determ	nination	s							Last Updated 47 H7/2005
GA	Oglethorpe Power Corp Wansley	521	01/15/2002	2	2	SW V84.3a2 (167 MW)	NG	СС	8,760	3.0 ppm	SCR		
GA	GenPower Rincon	528	03/24/2003	2	2	GE 7FA (170 MW)	NG	СС	8,760	2.5 ppm	SCR		
GA	Effingham Power Co.	525	12/27/2001	2	0	GE 7FA (170 MW)	NG	sc/cc	8,760	12/3.5 ppm	DLN/SCR		Initially SC, but later converting to CC
GA	Peace Valley Generation Co., LLC	1,550	draft permit	6	4	GE 7FA (170 MW)	NG	cc/sc	8,760/2, 500	2.5/9.0 ppm	SCR/DLN	3-hr	
GA	Savannah Electric and Power - Plant McIntosh	1,260	04/17/2003	4	4	GE 7FA (170 MW)	NG; FO	СС	8,760; 1,000 FO	2.5 ppm NG; 6 ppm FO	SCR		After June 1, 2007 - FO m have < 0.0015%S (ultra lov diesel)
GA	Live Oak Co., LLC	600	applic. under review	2	2	5W 501FD (170 MW)	NG	СС	8,760	3.5 ppm	SCR		
GA	Big River Power, LLC	855	applic. under review	3	3	GE 7FA (170 MW)	NG; FO	СС	8,760; 500 FO	3.0 ppm NG; 8.0 ppm FO	SCR/DLN; WI		SCR - \$5,075/ton NOx; Ca - \$4,712/ton CO
KV	Kantuska Blancas Engana	540	00/00/0004	_	_	GE 7FA	synga		0.700	45/00	Steam	2 hr	
KY	Kentucky Ploneer Energy	540	06/08/2001	2	0	(197 MW)		CC	8,760	15/20 ppm	Injection	3-hr	
KY	Duke Energy Trimble	1,240	applic. under review	4	4	GE 7FA (160 MW)	NG; FO	СС	8,760; 1,000 FO	3.5 ppm	SCR		
MS	LS Power, LP (Batesville)	1,100	11/07/1999	3	3	SW 501G (281 MW)	NG; FO	СС	8,760 (10% FO)	9 ppm NG; 42 ppm FO	DLN; WI		
MS	Mississippi Power Corp., Plant Daniel	1,000	12-98	4	4	GE 7FA (170 MW)	NG	CC	8,760	3.5 ppm / 0.018 lb/MMBtu	DLN/SCR		
MS	Duke Energy Hinds, L.L.C.	520	01/07/2000	2	0	GE 7FA (170 MW)	NG	ĊC	8,760	3.5 ppm	DLN/SCR		
MS	Duke Energy Attala, L.L.C.	520	4-00	2	0	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm	DLN/SCR		
MS	Cogentrix Energy, Southaven Power Project	800	04/25/2000	3	3	GE 7FA (170 MW)	NG	СС	8,760	4.5 ppm (10.8 ppm w/ DB)	DLN/SCR		
MS	Cogentrix Energy, Caledonia Power Project	800	3-01	3	3	GE 7FA (182 MW)	NG	СС	8,760	3.5 ppm (w/DB)	DLN/SCR		revised application to ad SCR
MS	GenPower - McAdams LLC	528	08/16/2000	2	2	GE 7FA (170 MW)	NG	cc	8,760	3.5 ppm	DLN/SCR	24-hr	
MS	Lone Oak Energy Center	800	11/13/2001	3	3	F" Class (180 MW)	NG	СС	8,760	3.5 ppm	SCR		Base/PA/PA+DF/DF
MS	Lee Power Partners	1,000	03/09/2001	4	4	F" Class (170 MW)	NG	СС	8,760	3.5 ppm	SCR		
MS	LSP-Pike Energy LLC	1,100	11/14/2000	4	4	F" Class (170 MW)	NG	СС	8,760	4.5 ppm	SCR		
MS	Magnolia Energy	900	05/31/2001	3	3	F" Class (170 MW)	NG	СС	8,760	3.5 ppm	SCR		
MS	Reliant Energy - Choctaw Co., LLC	844	06/13/2001	3	3	GE 7FA (170 MW)	NG	CC	8,760	3.5 ppm	DLN, SCR	30- day	SCONOx - \$48,663/ton No CatOx - \$3,550/ton CO
						GE 7FA						1	SCONOx - \$23,400/ton No

GE 7FA (170 MW) SW 501G (250 MW)

06/24/2002

12/13/2001

2

2

2

2

580

700

Crossroads Energy Center

Choctaw Gas Generation, LLC

MS

MS

NG

NG

CC

CC

8,760

8,760

3.5 ppm

3.5 ppm

SCR

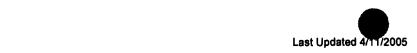
SCR

CatOx - \$11,039/ton CO

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MS	LSP Energy (Granite Power)	300	11/13/2001	1	1	SW 501F (230 MW)	NG	СС	8,760	3.5 ppm	SCR	3-hr	
MS	Panada Black Prairie LP	1,040	applic, under review	4	4	F" Class (175 MW)	NG	СС	8,760	3.5 ppm	SCR	24-hr	GE7FA or SW501F
NC	Carolina Power & Light, Richmond Co. (2nd revision - new configuration)	2,040	applic, under review	9	0	GE 7FA (170 MW)	NG; FO	cc/sc	8,760/2, 000; 1,000 FO	-3.5/9 ppm NG; 13/42 ppm FO	SCR/DLN; SCR/WI	24-hr	Reconfiguration of facility: 6 CC and 3 SC CTs
NC	Carolina Power & Light, Rowan Co. (revision)	1,110	draft permit	2	0	GE 7FA (170 MW)	NG; FO	СС	8,760; 1,000 FO	9 ppm NG; 42 ppm FO	DLN; WI		Modification of previous permit to switch 2 SC -> CC
NC	Fayetteville Generation	500	01/10/2002	2	0	GE 7FA (170 MW)	NG; FO	cc/sc	8,760; 1000 FO	2.5/9 ppm NG; 13/42 ppm FO	SCR/DLN; SCR/WI		CO level for FO depends on Load
NC	GenPower Earleys, LLC	528	01/14/2002	. 2	2	GE 7FA (170 MW)	NG	СС	8,760	2.5/3.5 ppm	SCR		CO Limit depends on CT model; NOx limit depends on operating history and 3.3 ppm trigger level SCONOx - \$21,942/ton NOx; CatOx - \$3,246ton CO
NC	Mirant Gastonia	1,200	05/28/2002	4	4	"F" Class (175 MW)	NG	· CC	8,760	2.5/3.5 ppm	SCR	24-hr block	operating history and 3.3 ppm trigger level
NC	Carolina Plant	1,300	applic. under review	4	4	GE or SW (170 MW)	NG; FO	СС	8,760	2.5/3.5 ppm; 13/18 ppm	SCR	24-hr block	CO Limit depends on CT model; NOx limit depends on operating history and 3.3 ppm trigger level
NC	Mountain Creek - Granville Energy Center	911	applic, under review	3	3	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm	SCR		SCONOx - \$22,600/ton NOx; CatOx - \$3,560ton CO
NC	Dominion Person, Inc.	1,100	applic, under review	4	4	GE 7FA (172 MW)	NG; FO	СС	8,760; 500 FO	3.5 ppm; 15 ppm FO	SCR		
NC	Forsyth Energy Projects	812	01/23/2004	3	3	GE 7FA (170 MW)	NG; FO	СС	8,760; 1200 FO	2.5/3.5 ppm NG; 13/18 ppm FO	SCR	24-hr block	CO Limit depends on CT model; NOx limit depends on operating history and 3.3/17 pm trigger levels
sc	Santee Cooper, Rainey Generating Station	870	4-00	4	0	GE 7FA (170 MW)	NG, FO	2 CC, 2 SC	8,760; 1,000 FO	9 ppm NG; 42 ppm FO	DLN; WI		
sc	SC Electric & Gas - Urquhart	444	9-00	2	0	GE 7FA (150 MW)	NG, FO	СС	8,760; 4,380 FO	45 ppm	DLN		Netted out of NOx, SO2 and PM10 PSD Review
sc	Columbia Energy	515	4-01	2	2	GE 7FA (170 MW)	NG, FO	cċ	8,760; 1,000 FO	3.5 ppm NG; 12 ppm FO	DLN/SCR; WI		SCONOx - no analysis; CatOx - \$1,611/ton CO
SC	GenPower Anderson	640	07/03/2001	2	2	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm	DLN/SCR		
sc	Greenville Power Project	810	applic. under review	3	3	GE 7FA (170 MW)	NG, FO	СС	8,760; 720 FO	3.5 ppm NG; 20 ppm FO	SCR		SCONOx - \$18,300/ton NOx; CatOx - \$5,800/ton CO; DB < 5,120 hr/yr
sc	Jasper County Generating Facility	1,260	05/28/2002	4	4	GE 7FA (170 MW)	NG, FO	СС	8,760; 720 FO	2.5 ppm NG; 7.5 ppm FO	SCR	24-hr	SCONOx - \$19,870/ton NOx; CatOx - \$3,320/ton CO





sc	Cherokee Falls Combined-Cycle Facility	1,260	applic. under review	4	4	GE 7FA (173 MW)	NG, FO	СС	8,760; 720 FO	3.5 ppm NG; 12 ppm FO	SCR		SCONOx - \$22,434/ton NOx; CatOx - \$2,500/ton CO
sc	Fork Shoals Energy, LLC	1,150	applic. under review	2	2	"F" Class (175 MW)	NG	cc	8,760	3.5 ppm	SCR	24-hr	
sc	Palmetto Energy Center	970	applic. under review	3	3	GE 7FB (180 MW)	NG	СС	8,760	3.5 ppm	SCR		SCONOx - \$18,789/ton NOx; CatOx - \$2,111/ton CO
TN	Vanderbilt University	10	5-00	2	2	GE PGT5B (5.2 MW)	NG	СС	8,760	25 ppm	DLN		
TN	Memphis Generation LLC	1,050	04/09/2001	4	0	GE 7FA (170 MW)	NG	СС	8,760	3.5 ppm	SCR		Phase I - 1 CT (up to 7% total plant heat input from refinery fuel gas), Phase II - 3 CTs (up to 2% total plant heat input from refinery fuel gas)
TN	Haywood Energy Center (Calpine)	900	02/01/2002	3	3	SW, GE 7FA or GE F7B	NG; FO	СС	8,760	3.5 ppm NG; 42 ppm FO	DLN/SCR; WI		
TN	TVA - Franklin	610	draft permit	2	2	GE 7FA (195 MW)	NG	СС	8,760	3.5 ppm	SCR		
TN	Southern Power Co.	1,940	applic. under review	8	4	GE 7FA (170 MW)	NG; FO	cc/sc	8760; 1,000 FO	3.5/9 ppm NG; 12/42 ppm FO	SCR/DLN: SCR/WI		

Abbreviations:

GE = General Electric

SW = Siemens Westinghouse

NG = Natural Gas

FO = Fuel Oil

SC = Simple Cycle

CC = Combined Cycle

DLN = Dry-Low NOx

WI = Water Injection

SCR = Selective Catalytic Reduction

Source: www.epa.gov/region4/air/permits

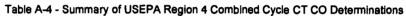






State	Facility	# of New MW	Final Permit issued	# of CTs	# of DB	Turbine Model	Fuel	Mode	Hours	CO Limit	Control Method	Avg. Time	Comments
Region 4													
AL	Alabama Power - Olin Cogeneration	137	12/01/1997	1	1	GE 7EA (80 MW)	NG	СС	8,760	0.07 lb/MMBtu	GCP		Power Augmentation
AL	Alabama Power - GE Plastics Cogeneration	100	05/01/1998	1	1	GE 7EA (80 MW)	NG	СС	8,760	0.08 lb/MMBtu (combined)	GCP		-
AL	Alabama Power, Plant Barry	800	08/01/1998	3	3	GE 7FA (170 MW)	NG	CC	8,760	0.057 lb/MMBtu	GCP		
AL	Alabama Power, Plant Barry	200	08/01/1999	1	1	GE 7FA (170 MW)	NG	CC	8,760	0.060 lb/MMBtu	GCP		
AL	Mobile Energy, LLC - Hog Bayou	200	1-99	1	1	GE 7FA (168 MW)	NG; FO	СС	8,760; 675 FO	0.040 lb/MMBtu NG; 0.058 lb/mmBtu FO	GCP		
AL	Alabama Power - Theodore Cogeneration Facility	210	3-99	1	1	GE 7FA (170 MW)	NG	СС	8,760	0.086 lb/MMBtu	GCP		
AL	Tenaska Alabama Partners	846	11-99	3	3	GE 7FA (170 MW)	NG; FO	СС	8,760; 720 FO	32.9 ppm NG; 46.7 ppm NG/FO	GCP	_	
AL	Georgia Power - Goat Rock	-	4-00	8	8	GE 7FA (170 MW)	NG	СС	8,760	0.086 lb/MMBtu	GCP		
AL	Georgia Power - Goat Rock (revision of above PSD application)	2,460	4-01	8	8	GE 7FA (170 MW)	NG	СС	8,760	0.086 lb/MMBtu	GCP		
AL	Alabama Electric Cooperative - Gantt Plant	500	3-00	2	2	SW 501F (166 MW)	NG	СС	8,760	0.057 lb/MMBtu	GCP		
AL	South Eastern Energy Corp.	1,500	1-01	6	в if СС	GE 7FA or SW 501F	NG	SC or CC	8,760	9 or 19 or 22 ppm	GCP		For NOx and CO: SC w/GE or SC w/SW501F or CC (either)
AL	Calpine Solutia - Decatur	700	6-00	3	3	SW501F (180 MW)	NG	СС	8,760	0.117 lb/mmBtu	GCP		
AL	Calpine BP Amoco	700	6-00	3	3	SW501F (180 MW)	NG	СС	8,760	0.117 lb/mmBtu	GCP		
AL	Tenaska Alabama II Generating Station	900	2-01	3	3	GE 7FA or Mitsubishi M501F	NG; FO	СС	8,760; 720 FO	0.037/0.047/0.089 Ib/mmbtu (base/PA/FO) - GE; 0.088/0.116/0.35 Ib/mmbtu (base/PA/FO) - Mit	GCP		
AL	Hillabee Energy Center	700	1-01	2	2	SW501G (229 MW)	NG	СС	8,760	0.023/0.076 lb/mmBtu (w/PA and/or DB)	GCP		PA = Power Augmentation, DB= Duct Burning
AL	Duke Energy - Alexander City	1,260	2-01	10	2	GE 7FA & 7EA	NG	CC & SC	8,760 CC; 2,500 SC	0.059 lb/mmBtu (130 lb/hr) CC; 0.09 lb/mmBtu (80 lb/hr) SC	GCP		8 SC units and 2 CC units
AL	GenPower - Kelly, LLC	1,260	1-01	4	4	GE 7FA (170 MW)	NG	СС	8,760	9 ppm, 14 ppm (w/DB)	GCP		
AL	Blount County Energy	800	1-01	3	3	"F" Class (170 MW)	NG	СС	8,760	0.033 lb/mmBtu (77.7 lb/hr)	GCP		
AL	Alabama Power - Autaugaville	1,260	1-01	4	4	"F" Class (170 MW)	NG	СС	8,760	0.035 lb/mmBtu	GCP		
AL	Tenaska Alabama IV Partners	1,840	10/09/2001	6	6	Mit 501F (170 MW)	NG; FO	СС	8,760; 720 FO	0.088 lb/mmBtu NG (0.115 w/PA & DB); 0.35 lb/mmBtu FO	GCP		SCONOx - \$6,145/ton NOX; CatOx- \$1,506/ton CO
AL	Duke Energy Autauga, LLC	630	10/29/2001	2	2	GE 7FA (170 MW)	NG	СС	8,760	15 ppm	GCP		SCONOx - \$18760/ton NOX; CatOx- \$5,006/ton CO





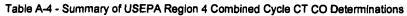


AL	Duke Energy Dale, LLC	630	12/17/2001	2	2	GE 7FA	NG	СС	8,760	0.033 lb/mmbtu	GCP	ļ	SCONOx - \$18,403/ton NOX;
AL	Barton Shoals Energy, LLC	1,200	07/15/2002	4	4	(170 MW) GE 7FA (170 MW)	NG	СС	8,760	10 ppm (0.022 lb/mmbtu); 0.041 lb/mmbtu w/DB	GCP		EPA did not received application until 5/24/02
FL	City of Lakeland, McIntosh Power Plant	250	7-10-98	1	0	SW 501G (230 MW)	NG; FO	SC (later CC)	7,008; 250 FO	25 ppm NG; 90 ppm FO	GCP		Power Augmentation
FL	Santa Rosa Energy Center, Sterling Fibers Mfg. Facility	241	12-4-98	1	1	GE 7FA (167 MW)	NG	СС	8,760	9 ppm; 24 ppm w/ DB	GCP		If a different CT is used, SCR may be required to meet 6 ppm NOx)
FL	Kissimmee Utility Authority, Cane Island Power Park -Unit 3	250	draft permit	1	0	GE 7FA (167 MW)	NG; FO	СС	8,760; 720 FO	12 ppm, 20 ppm w/ DB NG; 30 ppm FO	GCP		
FL	Duke Energy - New Smyrna Beach	500	draft permit	2	0	GE 7FA (165 MW)	NG	СС	8,760	12 ppm	GCP		
FL	City of Tallahassee - Purdom	250	5-98	1	Ó	GE 7FA (160 MW)	NG; FO	СС	8,760	25 ppm NG; 90 ppm FO	GCP	3-hr test	
FL	Gulf Power - Smith Station	340	7-00	2	2	GE 7FA (170 MW)	NG	СС	8,760	16 ppm w/ DB, 23 ppm w/ DB & SA	GCP		Netting out of PSD for NOx and CO; SA = steam augmentation
FL	Florida Power & Light - Sanford	2,200	9-99	8	0	GE 7FA (170 MW)	NG, FO	СС	8,760; 500 FO	12 ppm NG; 20 ppm FO	GCP		Repowering, 4 units FO
FL	Gainesville Regional Utilities, Kelly Generating Station	133	2-00	1	0	GE 7EA (83 MW)	NG; FO	СС	8,760; 1,000 FO	20 ppm NG; 20 ppm FO	GCP		Netting out of PSD review for NOx
FL	Calpine Osprey Energy Center	. 527	07/05/2001	2	2	5W 501FD (170 MW)	NG	СС	8,760	10 ppm (17 ppm w/DB or PA)	GCP	24-hr Block	2,800 hr/yr - Power Aug. mode
FL	Hines Energy ( FPC)	530	06/07/2001	2	0	SW 501FD (170 MW)	NG; FO	СС	8,760; 1,000 FO	16 ppm NG; 30 ppm FO	GCP	24-hr Block	SCONOx - \$16,712/ton NOx.; CatOx - \$2,130/ton CO
FL	CPV - Gulfcoast	250	2-01	1	0	GE 7FA (170 MW)	NG; FO	СС	8,760; 720 FO	9 ppm NG; 20 ppm FO	GCP		SCONOx - no cost eval.; CatOx - \$4,350/ton CO
FL	TECO Gannon/Bayside	1,728	3-01	7	0	GE 7FA (170 MW)	NG; FO	СС	8,760; 876 FO	7.2 ppm NG; 14.2 ppm FO	GCP		Repowering project: netting out of NOx, CO, PM10 and SO2 review (subject to VOC reveiw)
FL	South Pond Energy Park	600	draft permit	3	0	GE 7FA (170 MW)	NG; FO	sc/cc	3,390/8, 760; 720 FO	9 ppm NG; 20 ppm FO	GCP	3-hr	2 SC CT and 1 CC CT also capable of operating in SC mode.
FL	North Pond Energy Park	430	applic. under review	2	0	GE 7FA (170 MW)	NG; FO	sc/cc	3,390/8, 760; 720 FO	9 ppm NG; 20 ppm FO	GCP		1 SC CT and 1 CC CT also capable of operating in SC mode.
FL	Calpine Blue Heron Energy Center	1,080	draft permit	4	4	SW 501F (170 MW)	NG	СС	8,760	10/15.6/38.5/50 ppm	GCP		base/duct burner/power aug./60-70% load; SCONOx - \$9,982/ton NOx; CatOx - \$1,553/ton CO
FL	Jacksonville Electric Authority - Brandy Branch (revision)	200	03/29/2002	0	2	GE 7FA (170 MW)		СС	8760; 288 FO	14 ppm	GCP	24-hr	Conversion of 2 SC units to 2 CC units
FL	CPV - Atlantic Power	250	05/03/2001	1	0	GE 7FA (170 MW)	NG; FO	СС	8,760; 720 FO	9 ppm NG (15 ppm w/PA) ; 20 ppm FO	GCP		PA = Power Augmentation

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1	

Orlando Utilities - Curtis H Stanton Energy Center	633	09/26/2001	2	2	GE 7FA (170 MW)	NG; FO	cc	8,760; 1000 FO	18.1 ppm NG (26.3 w/PA): 14.3 ppm FO	GCP		
Broward Energy Center	775	05/15/2002	4	0	GE 7FA (175 MW)	NG	cc/sc	8,760/5, 000	8 ppm (SC & CC); 12	GCP	3-hr	SC; PA = Power
Belle Glade Energy Center	600	01/28/2002	3	0	GE 7FA (175 MW)	NG	CC/SC	8,760/5, 000	(SC); 14 ppm (CC	GCP	3-hr	SC; PA = Power
Manatee Energy Center	600	01/17/2002	3	0	GE 7FA	NG	cc/sc	8,760/5,	2.5 ppm/8 ppm; 4 ppm (CC w/PA)	GCP	3-hr	SC; PA = Power
CPV Pierce Power Generation Facility	250	08/17/2001	1	0	GE 7FA (170 MW)	NG; FO	СС	8,760; 720 FO	8 ppm NG (13 ppm w/PA); 17 ppm FO (19 ppm 76-89% load, 26 ppm 50-75% load)	GCP	24-hr	PA limited to 2,000 hr/yr
Fort Pierce Repowering Project	180	08/15/2001	1	1	SW 501F (180 MW)	NG; FO	CC/SC	8,760; 1,000 FO/2,00 0; 500 FO	3.5 ppm NG; 10 ppm FO/ 16 ppm NG; 50 ppm FO	GCP		CT will operate in both CC and SC modes
TECO Bayside Power Station (repowering)	1,032	01/09/2002	4	0	GE 7FA (170 MW)	NG	СС	8,760	9 ppm (7.8 ppm test avg.)	GCP	24-hr	Repowering Project: Netting out of PSD for NOx, SO2, lead and SAM (subject for PM10, VOC and CO)
CPV Cana Power Generation Facility	245	01/17/2002	1	1	GE 7FA (170 MW)	NG; FO	СС	8,760; 720 FO	8 ppm NG (13 ppm w/PA) ; 17/19/26 ppm FO	GCP	24-hr	PA limited to 2,000 hr/yr, CO
FPL Martin	1,150	04/16/2003	4	0	GE 7FA (170 MW)	NG; FO	CC/SC	8,760; 5000 FO/1,00 0; 500 FO	10 ppm NG/8 ppm NG (12 ppm w/PA); 15 ppm FO	GCP	24-hr	PA = Power Augmentation
FPL Manatee	1,150	04/15/2003	4	4	GE 7FA (170 MW)	NG	cc/sc	8,760/1, 000	10 ppm NG/8 ppm NG (12 ppm w/PA)	GCP	24-hr	PA = Power Augmentation
FPC - Hines Energy Complex	530	09/19/2003	2	0	5W 501FD (170 MW)	NG; FO	СС	8,760; 720 FO	10 ppm NG/20 ppm FO	GCP	24-hr	SCONOx - \$8,597/ton NOx;
FPL Turkey Point	1,150	draft permit	. 4	4	GE 7FA (170 MW)	NG; FO	СС	8,760; 500 FO	4.1 ppm NG/7.6 ppm NG w/DB/8 ppm NG w/PA&DB/14ppm w/PK&DB 8.0 ppm FO	GCP	24-hr	SCR (3.5ppm) = \$3,744/ton NOx; SCR (2.5 ppm) = \$3,753/ton NOx
Georgia Power - Wansley (Oglethorpe Power)	2,280	07/28/2000	8	8	GE 7FA (170 MW)	NG	СС	8,760	29.5 ppm/0.066 lb/MMBtu	GCP		-
Duke Energy Murray, LLC	1,240	2-01	4	4	GE 7FA (170 MW)	NG	сс	8,760	12 ppm*	GCP		NOx and CO BACT limits were lowered from 3.5 ppm and 22 ppm after the permit was issued in response to a settlement with an Environmental Group
Duke Energy Buffalo Creek, LLC	620	applic. under	2	2	GE 7FA (170 MW)	NG	СС	8,760	21.9 ppm	GCP		SCONOx - \$19,948/ton NOx; CatOx - \$2,469/ton CO
Augusta Energy LLC	750	09/28/2001	3	3	GE 7FA (170 MW)	NG; FO	СС	8,760; 1,000 FO	2 ppm NG; 2 ppm FO	CatOx		SCONOx - \$17,490/ton NOx; CatOx - \$1,828/ton CO
	Stanton Energy Center Broward Energy Center Belle Glade Energy Center Manatee Energy Center CPV Pierce Power Generation Facility  Fort Pierce Repowering Project  TECO Bayside Power Station (repowering)  CPV Cana Power Generation Facility  FPL Martin  FPL Manatee  FPC - Hines Energy Complex  FPL Turkey Point  Georgia Power - Wansley (Oglethorpe Power)  Duke Energy Murray, LLC  Duke Energy Buffalo Creek, LLC	Stanton Energy Center Broward Energy Center  Belle Glade Energy Center  Manatee Energy Center  CPV Pierce Power Generation Facility  Fort Pierce Repowering Project  180  TECO Bayside Power Station (repowering)  CPV Cana Power Generation Facility  1,032  CPV Cana Power Generation Facility  1,150  FPL Martin  1,150  FPL Manatee  1,150  FPC - Hines Energy Complex  530  FPL Turkey Point  1,150  Georgia Power - Wansley (Oglethorpe Power)  Duke Energy Murray, LLC  1,240  Duke Energy Buffalo Creek, LLC  620	Stanton Energy Center         633         09/26/2001           Broward Energy Center         775         05/15/2002           Belle Glade Energy Center         600         01/28/2002           Manatee Energy Center         600         01/17/2002           CPV Pierce Power Generation Facility         250         08/17/2001           Fort Pierce Repowering Project         180         08/15/2001           TECO Bayside Power Station (repowering)         1,032         01/09/2002           CPV Cana Power Generation Facility         245         01/17/2002           FPL Martin         1,150         04/16/2003           FPL Manatee         1,150         04/15/2003           FPC - Hines Energy Complex         530         09/19/2003           FPL Turkey Point         1,150         draft permit           Georgia Power - Wansley (Oglethorpe Power)         2,280         07/28/2000           Duke Energy Murray, LLC         1,240         2-01           Duke Energy Buffalo Creek, LLC         620         applic. under review	Stanton Energy Center         833         09/26/2001         2           Broward Energy Center         775         05/15/2002         4           Belle Giade Energy Center         800         01/28/2002         3           Manatee Energy Center         600         01/17/2002         3           CPV Pierce Power Generation Facility         250         08/17/2001         1           Fort Pierce Repowering Project         180         08/15/2001         1           TECO Bayside Power Station (repowering)         1,032         01/09/2002         4           CPV Cana Power Generation Facility         245         01/17/2002         1           FPL Martin         1,150         04/16/2003         4           FPL Manatee         1,150         04/15/2003         4           FPC - Hines Energy Complex         530         09/19/2003         2           FPL Turkey Point         1,150         draft permit         4           Georgia Power - Wansley (Oglethorpe Power)         2,280         07/28/2000         8           Duke Energy Buffalo Creek, LLC         620         applic. under review         2	Stanton Energy Center   833   09/26/2001   2   2	Stanton Energy Center   633   09/26/2001   2   2   (170 MW)	Stanton Energy Center   633   09/26/2001   2   2   (170 MW)   FO	Stanton Energy Center   633   09/26/2001   2   2   (170 MW)   FO   CC	Stanton Energy Center   6-33   09/26/2001   2   2   (170 MW)   FO   CC   10000 FO	Stanton Energy Center   6-33   694/26/2010   2   2   (170 MW)   FO   CC   1000 FO   (MPA) 1/4.3 ppm FO	Stanton Energy Center   9.3   09/26/2001   2   2   (170 MW)   FO   CC   1000 Fe   w/FA); 14.3 ppm FO   GCP	Salation Energy Centier   95.3   09/20/20/10   2   2   (170 MW)   FO   CC   1000 FO   w/FA), 14.3 ppm FO   GCP



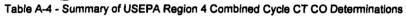




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GA	Oglethorpe Power Corp Wansley	521	01/15/2002	2	2	SW V84.3a2 (167 MW)	NG	СС	8,760	2.0 ppm	CatOx		
GA	GenPower Rincon	528	03/24/2003	2	2	GE 7FA (170 MW)	NG	СС	8,760	2.0 ppm	CatOx		
GA	Effingham Power Co.	525	12/27/2001	2	0	GE 7FA (170 MW)	NG	sc/cc	8,760	9 ppm	GCP		Initially SC, but later converting to CC
GA	Peace Valley Generation Co., LLC	1,550	draft permit	6	4	GE 7FA (170 MW)	NG	cc/sc	8,760/2, 500	2.0 ppm/8.0 ppm	CatOx/G CP	3-hr	
GA	Savannah Electric and Power - Plant McIntosh	1,260	04/17/2003	4	4	GE 7FA (170 MW)	NG; FO	СС	8,760; 1,000 FO	2.0 ppm	CatOx		After June 1, 2007 - FO must have < 0.0015%S (ultra low S diesel)
GA	Live Oak Co., LLC	600	applic. under review	2	2	5W 501FD (170 MW)	NG	СС	8,760	10 ppm (17 ppm w/DB or PA)	GCP		
GA	Big River Power, LLC	855	applic. under review	3	3	GE 7FA (170 MW)	NG; FO	СС	8,760; 500 FO	19.2 ppm (w/DB)/9.0 ppm (w/o DB) NG; 20.0 ppm FO	GCP		SCR - \$5,075/ton NOx; CatOx - \$4,712/ton CO
KY	Kentucky Pioneer Energy	540	06/08/2001	2	0	GE 7FA	synga	СС	8,760	15/20 ppm	GCP	3-hr	
					-	(197 MW)	s/NG		8,760;	10/20 pp			
кү	Duke Energy Trimble	1,240	applic. under review	4	4	GE 7FA (160 MW)	NG; FO	СС	1,000 FO	9/13.9/20 ppm	GCP		
									0.700			<u> </u>	
мѕ	LS Power, LP (Batesville)	1,100	11/07/1999	3	3	SW 501G (281 MW)	NG; FO	СС	8,760 (10% FO)_	30.3 ppm NG; 36 ppm FO	GCP		
MS	Mississippi Power Corp., Plant Daniel	1,000	12-98	4	4	GE 7FA (170 MW)	NG	СС	8,760	0.057 lb/MMBtu	GCP		
MS	Duke Energy Hinds, L.L.C.	520	01/07/2000	2	0	GE 7FA (170 MW)	NG	СС	8,760	20 ppm	GCP	,	
мѕ	Duke Energy Attala, L.L.C.	520	4-00	2	0	GE 7FA (170 MW)	NG	СС	8,760	20 ppm	GCP		
MS	Cogentrix Energy, Southaven Power Project	800	04/25/2000	3	3	GE 7FA (170 MW)	NG	СС	8,760	9 ppm, 18 ppm w/ DB	GCP		
MS	Cogentrix Energy, Caledonia Power Project	800	3-01	3	3	GE 7FA (182 MW)	NG	СС	8,760	9 ppm	GCP		revised application to add SCR
MS	GenPower - McAdams LLC	528	08/16/2000	2	2	GE 7FA (170 MW)	NG	СС	8,760	7-8 ppm/13 ppm (w/DB)	GCP	24-hr	
MS	Lone Oak Energy Center	800	11/13/2001	3	3	F" Class (180 MW)	NG	СС	8,760	10/25/30/17 ppm	GCP		Base/PA/PA+DF/DF
MS	Lee Power Partners	1,000	03/09/2001	4	4	F" Class (170 MW)	NG	СС	8,760	25 ppm	GCP		
MS	LSP-Pike Energy LLC	1,100	11/14/2000	4	4	F" Class (170 MW)	NG	СС	8,760	33.1 ppm (0.15 lb/mmBTU)	GCP		
MS	Magnolia Energy	900	05/31/2001	3	3	F" Class (170 MW)	NG	СС	8,760	25 ppm	GCP		
MS	Reliant Energy - Choctaw Co., LLC	844	06/13/2001	3	3	GE 7FA (170 MW)	NG	СС	8,760	18.36 ppm	GCP		SCONOx - \$48,663/ton NOx; CatOx - \$3,550/ton CO
MS	Crossroads Energy Center	580	06/24/2002	2	2	GE 7FA (170 MW)	NG	СС	8,760	10.4 ppm	GCP		SCONOx - \$23,400/ton NOx; CatOx - \$11,039/ton CO

MS	Choctaw Gas Generation, LLC	700	12/13/2001	2	2	SW 501G (250 MW)	NG	СС	8,760	23 ppm	GCP		
MS	LSP Energy (Granite Power)	300	11/13/2001	1	1	SW 501F (230 MW)	NG	СС	8,760	25 ppm	GCP	3-hr	
MS	Panada Black Prairie LP	1,040	applic. under review	4	4	F" Class (175 MW)	NG	СС	8,760	7.6 ppm or 80 ppm	GCP		GE7FA or SW501F
NC	Carolina Power & Light, Richmond Co. (2nd revision - new configuration)	2,040	applic, under review	9	0	GE 7FA (170 MW)	NG; FO	CC/SC	8,760/2, 000; 1,000 FO	9 ppm NG; 20 ppm FO	GCP		Reconfiguration of facility: 6 CC and 3 SC CTs
NC	Carolina Power & Light, Rowan Co. (revision)	1,110	draft permit	2	0	GE 7FA (170 MW)	NG; FO	СС	8,760; 1,000 FO	15 ppm NG; 20 ppm FO	GCP		Modification of previous permit to switch 2 SC -> CC
NC	Fayetteville Generation	500	01/10/2002	2	0	GE 7FA (170 MW)	NG; FO	cc/sc	8,760; 1000 FO	9 ppm NG; 20-41 ppm FO	GCP		CO level for FO depends on Load
NC	GenPower Earleys, LLC	528	01/14/2002	2	2	GE 7FA (170 MW)	NG	cc	8,760	9 ppm (14 ppm w/DB)	GCP		CO Limit depends on CT model; NOx limit depends on operating history and 3.3 ppm trigger level SCONOx - \$21,942/ton NOx; CatOx - \$3,246ton CO
NC	Mirant Gastonia	1,200	05/28/2002	4	4	"F" Class (175 MW)	NG	СС	8,760	15 or 30 ppm	GCP	24-hr block	
NC	Carolina Plant	1,300	applic. under review	4	4	GE or SW (170 MW)	NG; FO	СС	8,760	47 or 50 ppm	GCP	24-hr block	
NC	Mountain Creek - Granville Energy Center	911	applic. under review	3	3	GE 7FA (170 MW)	NG	СС	8,760	9 ppm (24.3 ppm w/DB)	GCP		SCONOx - \$22,600/ton NOx; CatOx - \$3,560ton CO
NC	Dominion Person, Inc.	1,100	applic, under review	4	4	GE 7FA (172 MW)	NG; FO	СС	8,760; 500 FO	9 ppm NG (20 ppm w/DB) 20 ppm FO	GCP		
NC	Forsyth Energy Projects	812	01/23/2004	3	3	GE 7FA (170 MW)	NG; FO	СС	8,760; 1200 FO	11.6 ppm NG (25.9 ppm w/DB); 15.7 ppm FO (25.1 ppm w/DB)	GCP	3-hr	CO Limit depends on CT model; NOx limit depends on operating history and 3.3/17 ppm trigger levels
sc	Santee Cooper, Rainey Generating Station	870	4-00	4	0	GE 7FA (170 MW)	NG, FO	2 CC, 2 SC	8,760; 1,000 FO	9 ppm NG; 20 ppm FO	GCP		
sc	SC Electric & Gas - Urquhart	444	9-00	2	0	GE 7FA (150 MW)	NG, FO	СС	8,760; 4,380 FO	12 ppm NG; 20 ppm FO	GCP		Netted out of NOx, SO2 and PM10 PSD Review
sc	Columbia Energy	515	4-01	2	2	GE 7FA (170 MW)	NG, FO	СС	8,760; 1,000 FO	17.4 ppm NG; 37 pm FO	GCP		SCONOx - no analysis; CatOx - \$1,611/ton CO
sc	GenPower Anderson	640	07/03/2001	2	2	GE 7FA (170 MW)	NG	СС	8,760	11.7 ppm	GCP		
sc	Greenville Power Project	810	applic. under review	3	3	GE 7FA (170 MW)	NG, FO	СС	8,760; 720 FO	12.3 ppm NG; 16.5 ppm FO	GCP		SCONOx - \$18,300/ton NOx; CatOx - \$5,800/ton CO; DB < 5,120 hr/yr







sc	Jasper County Generating Facility	1,260	05/28/2002	4	4	GE 7FA (170 MW)	NG, FO	СС	8,760; 720 FO	9 ppm NG (14 ppm w/DB); 20 ppm FO (22 ppm w/DB)	GCP		SCONOx - \$19,870/ton NOx; CatOx - \$3,320/ton CO
sc	Cherokee Falls Combined-Cycle Facility	1,260	applic. under review	4	4	GE 7FA (173 MW)	NG, FO	СС	8,760; 720 FO	0.063 lb/mmbtu NG; 0.069 lb/mmbtu FO	GCP		SCONOx - \$22,434/ton NOx; CatOx - \$2,500/ton CO
sc	Fork Shoals Energy, LLC	1,150	applic. under review	2	2	"F" Class (175 MW)	NG	СС	8,760	14 ppm (GE7FA/16 ppm (SW501F)	GCP	24-hr	
sc	Palmetto Energy Center	970	applic. under review	3	3	GE 7FB (180 MW)	NG	СС	8,760	15 ppm (31 ppm w/DB)	GCP		SCONOx - \$18,789/ton NOx; CatOx - \$2,111/ton CO
TN	Vanderbilt University	10	5-00	2	2	GE PGT5B (5.2 MW)	NG	СС	8,760	25 ppm	GCP		
TN	Memphis Generation LLC	1,050	04/09/2001	4	0	GE 7FA (170 MW)	NG	СС	8,760	0.03 lb/mmBtu	GCP		Phase I - 1 CT (up to 7% total plant heat input from refinery fuel gas), Phase II - 3 CTs (up to 2% total plant heat input from refinery fuel gas)
TN	Haywood Energy Center (Calpine)	900	02/01/2002	3	3	SW, GE 7FA or GE F7B	NG; FO	СС	8,760	varies from 7.4 to 50 ppm depending on CT type and load	GCP		
TN	TVA - Franklin	610	draft permit	2	2	GE 7FA (195 MW)	NG	СС	8,760	25 ppm	GCP		
TN	Southern Power Co.	1,940	applic. under review	8	4	GE 7FA (170 MW)	NG; FO	cc/sc	8760; 1,000 FO	0.035 lb/mmbtu NG; 0.069 lb/mmbtu FO	GCP		

Abbreviations:

GE = General Electric

SW = Siemens Westinghouse

NG = Natural Gas

FO = Fuel Oil

SC = Simple Cycle

CC = Combined Cycle

DLN = Dry-Low NOx

WI = Water Injection

SCR = Selective Catalytic Reduction

Source: www.epa.gov/region4/air/permits

# Appendix F Dispersion Modeling Protocol



11401 Lamar Avenue Overland Perk, Kansas 66211 USA Black & Vestch Corporation

Tel: (913) 458-2000

Florida Municipal Power Agency Treasure Coast Energy Center Unit 1 B&V Project 138859 B&V File 32.1100 B&V Letter No. BV/TP-0002 Date: January 7, 2005

Al Linero
Florida Department of Environmental Protection
Bureau of Air Regulation
Twin Towers Office Building
2600 Blair Stone Road
Tallahassee, Florida 32399-2400

Subject:

Treasure Coast Energy Center
Combined Cycle Unit 1 Project C

Combined Cycle Unit 1 Project Class II and Class I Air Dispersion Modeling

**Protocols** 

The Florida Municipal Power Agency (FMPA) is implementing the installation of a Nominal Net 310 MW 1x1 F-Class combined cycle unit (Project) at the new Treasure Coast Energy Center near Fort Pierce, FL.

Since the proposed Project will result in emissions greater than the major source threshold for at least one prevention of significant deterioration (PSD) pollutant, the PSD significant emission levels (SELs) will apply to the project. As such, the Project will be considered a new PSD major stationary source by the Florida Department of Environmental Protection (FDEP). It is anticipated that the proposed Project will be major for the following pollutants: NO_x, CO, SO₂, VOC, PM/PM₁₀, and sulfuric acid mist; thereby requiring PSD review for those pollutants. As part of that review, an air dispersion modeling demonstration must be performed to ensure that the proposed Project will comply with the appropriate ambient air quality thresholds in the surrounding areas.

Prior to such demonstration, the enclosed air dispersion modeling protocols have been developed for your review in an effort to obtain concurrence with the proposed modeling

the imagine - build company**

Florida Municipal Power Agency
Treasure Coast Energy Center Unit 1

B&V Project 138859 B&V File 32.1100 B&V Letter No. BV/TP 0002 January 7, 2005

methodologies. The modeling methodologies presented in this document were discussed with FDEP personnel at a pre-application meeting held at the FDEP offices in Tallahassee on December 15, 2004. We look forward to your concurrence with this modeling methodology at your earliest convenience. If you have any questions or comments, please feel free to contact me at 913-458-7928.

Regards,

**BLACK & VEATCH** 

Tim Hillman

**Senior Air Quality Scientist** 

#### **Attachments**

CC:

Rick Casey - FMPA
Kevin Fleming - FMPA
Susan Schumann - FMPA
Stanley Armbruster - B&V
Myron Rollins - B&V
Mike Soltys - B&V
Bob Holmes - B&V
File

### FLORIDA MUNICIPAL POWER AGENCY TREASURE COAST ENERGY CENTER COMBINED CYCLE UNIT 1

### CLASS II AND CLASS I AIR DISPERSION MODELING PROTOCOLS

PREPARED BY BLACK & VEATCH

**JANUARY 2005** 

### **ATTACHMENT 1**

# FLORIDA MUNICIPAL POWER AGENCY TREASURE COAST ENERGY CENTER COMBINED CYCLE UNIT 1

### ISC CLASS II MODELING PROTOCOL

PREPARED BY BLACK & VEATCH

**JANUARY 2005** 

### Air Quality Modeling Assumptions and Methodology

Modeling Scenario: As a new major stationary source, the air quality impact

analysis (AQIA) will be performed for Unit 1, a nominally rated 310 MW (net) 1x1 combined cycle unit to be installed at the new Treasure Coast Energy Center site near Fort Pierce, St. Lucie County, Florida. The location of the

proposed project is illustrated in the attached Figure.

Air Dispersion Model: ISCST3 (Latest version)

Model Options: USEPA Default and Flat terrain.

GEP & Downwash: USEPA's BPIP program will be used to determine GEP

stack height and direction specific building downwash parameters for the Unit 1 stack. Structures associated with

the new site will be included in the BPIP analysis.

Receptor Grids: A 10 km nested rectangular receptor grid consisting of 100

m spacing out to 1 km, 250 m spacing from 1 km to 2.5 km, 500 m spacing from 2.5 km to 5 km, and 1,000 m spacing from 5 km to 10 km. Fenceline receptors will be placed at 100 m intervals, and a 100 m fine grid will be

placed at maximum impact locations.

Dispersion Coefficients: Rural: Based on visual inspection of a 7.5 minute USGS

topographic map of the site using the Auer method.

Meteorological Data: Refined level modeling sequential hourly meteorological

data will consist of surface data and upper air data from the West Palm Beach Morrison Field (No. 12844) met station for the years 1987-1991. The files will be obtained from the Support Center for Regulatory Air Models website and processed with the USEPA meteorological processor

PCRammet.

Pollutants to be Modeled: The pollutants that are currently expected to be modeled

are PM₁₀, NO_x, SO₂, and CO.

Source Modeling Parameters: Representative combustion turbine performance and

emissions data for the several operating configurations; including natural gas firing, fuel oil firing with water injection, evaporative cooling, and duct firing. The performance and emission data will be determined across 50, 75, and 100 percent load cases at ambient temperatures of 26, 59, 73, and 100 °F. Enveloping will be used to

determine the worst-case hourly emission rates and operating parameters for each load case that will be used for short-term modeling impacts. Emission rates and operating parameters for annual modeling impacts will be based on annual average data, at 100 percent load.

Modeled impacts:

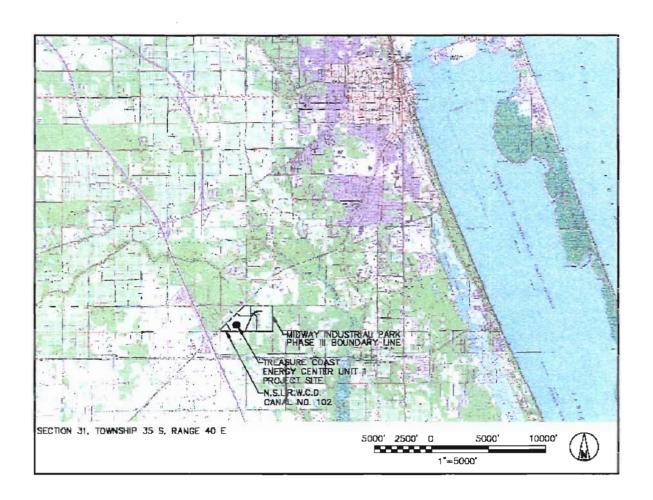
It is anticipated that the maximum model predicted pollutant impacts will be less than their respective PSD SILs. If the model predicted impacts exceed the SILs, additional agency consultation will be initiated regarding increment and cumulative air quality impact analyses.

Class I Analysis:

For analysis of the Everglades National Park Class I area, which lies beyond 50 km from the proposed project, the CALPUFF model will be used. The CALPUFF modeling protocol is discussed in Attachment 2 of this submittal.

Toxics:

No toxic modeling analysis is required.



Treasure Coast Energy Center Unit 1
Proposed Project Location

### **ATTACHMENT 2**

# FLORIDA MUNICIPAL POWER AGENCY TREASURE COAST ENERGY CENTER COMBINED CYCLE UNIT 1

### **CALPUFF CLASS I MODELING PROTOCOL**

PREPARED BY BLACK & VEATCH

**JANUARY 2005** 

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#### 1.0 Introduction

As part of the air impact evaluation for the proposed Treasure Coast Energy Center's Combined Cycle Unit 1 (hereinafter referred to as the Project), analyses of the proposed project's effect on the Everglades National Park (ENP) will be performed. The ENP is a Prevention of Significant Deterioration (PSD) Class I area located in southern Florida approximately 180 km south-southwest of the proposed project site. Federal Class I areas are afforded special environmental protection through the use of Air Quality Related Values (AQRVs). The AQRVs of interest in this protocol are regional haze and deposition. Additionally, Class I Significant Impact Levels (SILs) will be evaluated and compared to the recommended thresholds. Figure 1-1 presents the location of the proposed project site with respect to the ENP.

The methodology of the refined CALPUFF analysis will closely follow those procedures recommended in the Interagency Workgroup on Air Quality Modeling (IWAQM) Phase II report dated December 1998 and the Phase I Federal Land Managers' Air Quality Related Values Workgroup (FLAG) report dated December 2000 where appropriate for model option selections. This protocol includes a discussion of the meteorological and geophysical databases to be used in the analysis, the preparation of those databases for introduction into the modeling system, and the air modeling approach to assess impacts at ENP.

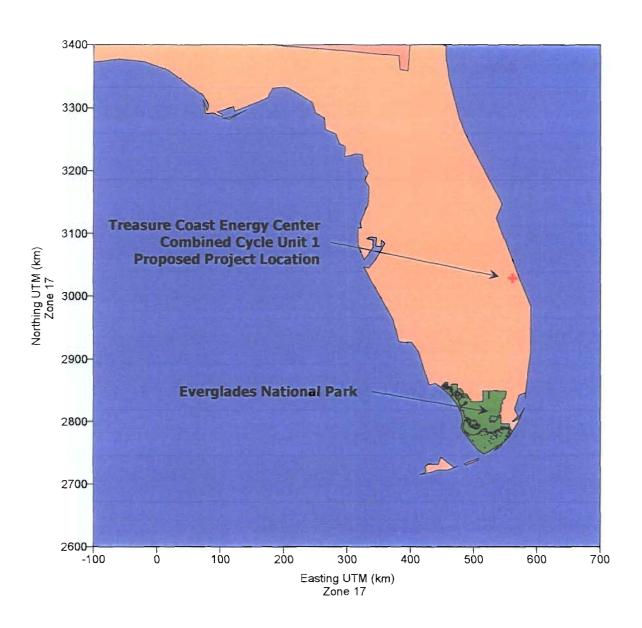


Figure 1-1 Proposed Project Location with respect to Everglades National Park

## 2.0 Model Selection and Inputs

#### 2.1 Model Selection

The California Puff (CALPUFF, Version 5.711A, Level 040716) air modeling system will be used to model the proposed project and assess the AQRVs at ENP. CALPUFF is a non-steady state Lagrangian Gaussian puff long-range transport model that includes algorithms for building downwash effects as well as chemical transformations (important for visibility controlling pollutants), and wet/dry deposition. The CALMET model, a preprocessor to CALPUFF, is a diagnostic meteorological model that produces three-dimensional fields of wind and temperature and two-dimensional fields of other meteorological parameters. CALMET was designed to process raw meteorological, terrain, and land-use databases to be used in the air modeling analysis. The CALPUFF modeling system uses a number of FORTRAN preprocessor programs that extract data from large databases and converts the data into formats suitable for input to CALMET. The processed data produced from CALMET will be input to CALPUFF to assess pollutant specific impacts.

## 2.2 CALPUFF Model Settings

The CALPUFF settings contained in Table 2-1 will be used for the modeling analyses.

#### 2.3 Building Wake Effects

The CALPUFF analysis will include the facility's building dimensions to account for the effects of building-induced downwash on the emission sources. Dimensions for all significant building structures will be processed with the Building Profile Input Program (BPIP), Version 95086, and included in the CALPUFF model input.

#### 2.4 Receptor Locations

The CALPUFF analysis will use an array of discrete receptors for ENP, which were created and distributed by the NPS for standardized use in Class I analyses. Terrain throughout the ENP is included in the same NPS- provided receptor file.

	Table 2-1		
CAL	PUFF Model Settings		
Parameter	Setting		
Pollutant Species	SO ₂ , SO ₄ , NO _x , HNO ₃ , and NO ₃ , and PM ₁₀		
Chemical Transformation	MESOPUFF II scheme		
Deposition	Include both dry and wet deposition, plume depletion		
Meteorological/Land Use Input	CALMET		
Plume Rise	Transitional plume rise, Stack-tip downwash,		
	Partial plume penetration		
Dispersion	Puff plume element, PG/MP coefficients, rural ISC		
	mode, ISC building downwash scheme		
Terrain Effects	Partial plume path adjustment		
Outside	Create binary concentration and wet/dry deposition		
Output	files including output species for all pollutants.		
Model Processing	Regional Haze:		
	Highest predicted 24-hour change as processed by		
	CALPOST.		
	Deposition:		
	Highest predicted annual total sulfur and nitrogen		
	values in deposition units.		
	Class I SILs:		
	Highest predicted concentrations at the applicable		
	averaging periods for those pollutants that exceed		
	the respective PSD Significant Emission Levels		
	(SELs).		
Background Values	Monthly Ammonia: 0.5 ppb;		
	Monthly background ozone will be based on a		
	review of the available monitoring stations' values		
	averaged for each month.		
	Additionally, hourly background ozone values from		
	several reporting stations may be assessed for		
	inclusion into the CALPUFF modeling.		

## 2.5 Meteorological Data Processing

The California Puff meteorological and geophysical data preprocessor (CALMET, Version 5.53A, Level 040716) will be used to develop the gridded parameter fields required for the refined AQRV modeling analyses. The following sections discuss the data to be used and processed in the CALMET model.

#### 2.5.1 CALMET Settings

The CALMET settings, including horizontal and vertical grid coverage and resolution of prognostic mesoscale meteorological data, will be chosen to adequately characterize the area within the CALMET domain.

#### 2.5.2 Modeling Domain

The size of the domain used for the modeling will be based on the distances needed to cover the area from the proposed project to the receptors at the ENP with at least a 50-km buffer zone in each direction. The modeling analysis will be performed in the UTM coordinate system. A rectangular modeling domain extending 215 km in the east-west (x) direction and 385 km in the north-south (y) direction will be used for the refined modeling analysis. The southwest corner of the domain is the origin and is located at 400 km Easting and 2,695 km Northing (based on UTM Zone 17, North American Datum (NAD) 1927 coordinates). The grid resolution for the domain will be 5 km. A grid spacing of 5 km yields 43 grid cells in the x-direction and 77 grid cells in the y-direction. Figure 2-1 illustrates the size and location of the modeling domain.

#### 2.5.3 Mesoscale Model Data

Pennsylvania State University in conjunction with the National Center for Atmospheric Research (NCAR) Assessment Laboratory have developed mesoscale meteorological data sets of prognostic wind fields, or "guess" fields, for the United States. The hourly meteorological variables used to create these data sets (wind, temperature, dew point depression, and geopotential height for eight standard levels and up to 15 significant levels) are extensive and are used to populate the modeling domain with meteorological data. The analysis will use 1990 MM4, 1992 MM5, and 1996 MM5 mesoscale meteorological data sets to initialize the CALMET wind fields for each modeled year. The three years of MM data will be obtained from a NPS database provided to Black & Veatch. The extraction program accompanying the data will be used to obtain the

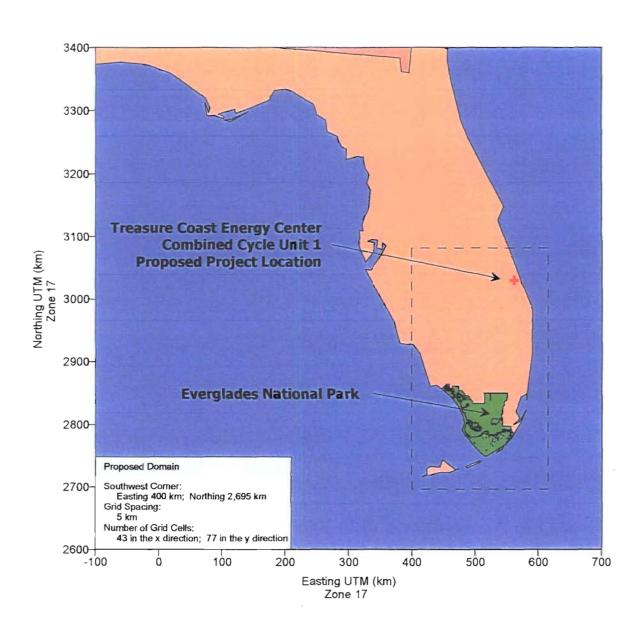


Figure 2-1 Proposed CALPUFF Modeling Domain

appropriate MM data points to cover the modeling domain. The 1990 MM4 and 1992 MM5 data have a horizontal spacing, or resolution, of 80 km. The 1996 MM5 data has a resolution of 36 km. The meteorological observations contained with the MM data sets are assumed to be of sufficient density, both temporally and spatially, to make the need for discrete meteorological station observation unnecessary. Thus, CALMET will be run with the No Observations mode developed in the latest version available from the model developer, EarthTech.

#### 2.5.4 Geophysical Data Processing

Terrain elevations for each grid cell of the modeling domain will be obtained from 1-degree Digital Elevation Model (DEM) files obtained from US Geographical Survey (USGS). The DEM data will be extracted for the modeling domain grid using the CALMET preprocessor program TERREL. Land-use data, based on annual averaged values, will also be obtained from the USGS. Land-use values for the domain grid will be extracted with the preprocessor programs CTGCOMP and CTGPROC. Other parameters processed for the modeling domain include surface roughness, surface albedo, Bowen ratio, soil heat flux, and leaf index field. Once preprocessed, all of the land-use parameters will be combined with the terrain information in a processor called MAKEGEO. This processor will produce one GEO.DAT file for input to CALMET.

#### 2.6 Project Emissions

The proposed Project will have the capability of operating in several configurations; including natural gas firing, fuel oil firing with water injection, evaporative cooling, and duct firing. The maximum pound per hour emission rates from Unit 1 at 100% load, across the several operating configurations, and the average annual temperature will be used for the pollutants modeled with CALPUFF. Those pollutants include NO_x, SO₂, and PM₁₀. Only emissions from Unit 1 will be assessed for long-range transport.

## 3.0 CALPUFF Analyses

The preceding model inputs and settings for the CALPUFF modeling system will be used to complete the Class I analyses on the ENP, including regional haze, deposition, and Class I SILs.

## 3.1 Regional Haze Analysis

A regional haze analysis will be performed for the ENP for ammonium sulfates, ammonium nitrates, and particulate matter by appropriately characterizing model predicted outputs of SO₄, NO₃, and PM₁₀ concentrations.

#### 3.1.1 Visibility

Visibility is an AQRV for the ENP. Visibility can take the form of plume blight for nearby areas, or regional haze for long distances (e.g., distances beyond 50 km). Because the ENP lies beyond 50 km from the proposed project, the change in visibility is analyzed as regional haze. Regional haze impairs visibility in all directions over a large area by obscuring the clarity, color, texture, and form of what is seen. Current regional haze guidelines characterize a change in visibility by either of the following methods:

- 1. Change in the visual range, defined as the greatest distance that a large dark object can be seen, or
- 2. Change in the light-extinction coefficient (bext).

Visual range can be related to extinction with the following equation:

$$b_{ext}(Mm^{-1}) = 3912 / vr(Mm^{-1})$$

Visual range (vr) is a measure of how far away a large black object can be seen in the atmosphere under several severe assumptions including: an absolutely dark target, uniform lighting conditions (cloud free skies), uniform extinction in all directions, a limiting contrast discrimination level, a target high enough in elevation to account for earth curvature, and several other factors. Visual range is, at best, a limited concept that allows relatively simple comparisons between visual air quality levels and should not be thought of as the absolute distance that can be seen through the atmosphere.

The b_{ext} is the attenuation of light per unit distance due to the scattering (light reduced away from the site path) and absorption (light captured by aerosols and turned into heat

energy) by gases and particles in the atmosphere. A change in the extinction coefficient produces a perceived visual change that is measured by a visibility index called the deciview. The deciview (dv) is defined as:

$$dv = 10 \ln (1 + b_{exts} / b_{extb})$$

where:

bexts is the extinction coefficient calculated for the source, and

bextb is the background extinction coefficient

A uniform incremental change in b_{extb} or visual range does not necessarily result in uniform changes in perceived visual air quality. In fact, perceived changes in visibility are best related to a percent change in extinction. Based on NPS guidance, if the change in extinction is less than 5 percent, no further analysis is required. An index similar to the deciview that simply quantifies the percent change in visibility due to the operation of a source is calculated as:

$$\Delta\% = (b_{\text{exts}} / b_{\text{extb}}) \times 100$$

#### 3.1.2 Background Visual Ranges and Relative Humidity Factors

The background visual range is based on data representative of historical conditions at the ENP. The background visual range, or constituents thereof, for the ENP will be obtained from the Phase I FLAG Report, December 2000. The average relative humidity factor for each day will be computed by determining the relative humidity factor for each hour's relative humidity for the 24-hour period that the impact occurred. This factor, based on each relative humidity will be obtained by using Table 2.A-1 of Appendix 2.A of the Phase I FLAG Report. These factors (a relative humidity factor for each relative humidity) will then be used to determine the average relative humidity factor for that day (24-hour period). All of this is accomplished with the use of the CALPOST post-processor.

#### 3.1.3 Interagency Workgroup On Air Quality Modeling (IWAQM) Guidelines

The CALPUFF air modeling analysis will closely follow the recommendations contained in the *IWAQM Phase II Summary Report and Recommendations for Modeling Long Range Transport Impacts*, (USEPA, 12/98) where appropriate. Table 3-1 summarizes the IWAQM Phase II recommendations. The methodology in Table 3-1 will be used to compute the results of the regional haze analysis. However, CALPOST now possesses the ability to

	Table 3-1
	Outline of IWAQM Refined Modeling Analyses Recommendations *
Meteorology	Use CALMET (minimum 6 to 10 layers in the vertical; top layer must extend
	above the maximum mixing depth expected); horizontal domain extends 50 to 80
	km beyond outer receptors and source being modeled; terrain elevation and land-
	use data is resolved for the situation.
Receptors	Within Class I area(s) of concern; NPS will provide the modeling receptors.
Dispersion	1. CALPUFF with default dispersion settings.
	2. Use MESOPUFF II chemistry with wet and dry deposition
	3. Define background values for ozone and ammonia for area
Processing	Use highest predicted 24-hr SO ₄ , PM ₁₀ and NO ₃ values; compute a day-average
	relative humidity factor (f(RH)) for the worst day for each predicted species,
	calculate extinction coefficients and compute percent change in extinction using
	the FLAG supplied background extinction where appropriate. This can all now
	be accomplished with the use of Method 2 in the CALPOST post-processor.
* IWAQM Pha	se II Summary Report and Recommendations for Modeling Long Range Transport
Impacts (USE	PA, 12/98).

post-process the modeling results specific to the regional haze analysis through the selection of one of seven modeling options. The post-processing selection will be made to calculate regional haze based on the appropriate available data/resources. Specifically, regional haze will be calculated using Method 2, which consists of computing extinctions from speciated PM measurements using hourly relative humidity adjustments for observed and modeled sulfate and nitrates. Based on recent correspondence with staff of the NPS for similar analyses, the relative humidity will be capped at 95 percent. A supplementary analysis will be performed with the relative humidity capped at 98 percent for informational purposes only. Method 7, which eliminates hours during which visibility limiting weather events occur, may be explored as necessary. While this process occurs within CALPOST, a typical calculation methodology is illustrated below.

#### Calculation

Refined impacts will be calculated as follows:

- Obtain 24-hour SO₄, NO₃, and PM₁₀ impacts, in units of micrograms per cubic meter (μg/m³).
- 2. Convert the SO₄ impact to (NH₄)₂SO₄ by the following formula:

 $(NH_4)_2SO_4 (\mu g/m^3) = SO_4 (\mu g/m^3) \times molecular weight (NH_4)_2SO_4 / molecular weight SO_4 (NH_4)_2SO_4 (\mu g/m^3) = SO_4 (\mu g/m^3) \times 132/96 = SO_4 (\mu g/m^3) \times 1.375$ 

Convert the NO₃ impact to NH₄NO₃ by the following formula:

 $NH_4NO_3 (\mu g/m^3) = NO_3 (\mu g/m^3) x$  molecular weight  $NH_4NO_3$  / molecular weight  $NO_3$   $NH_4NO_3 (\mu g/m^3) = NO_3 (\mu g/m^3) x$   $80/62 = NO_3 (\mu g/m^3) x$  1.29

3. Compute b_{exts} (extinction coefficient calculated for the source) with the following formula:

$$b_{exts} = 3 \times NH_4NO_3 \times f(RH) + 3 \times (NH_4)_2SO_4 \times f(RH) + 1 \times PM_{10}$$

4. Compute b_{extb} (background extinction coefficient) using the background visual range (km) from the FLAG document with the following formula:

 $b_{extb} = 3.912 / Visual range (km)$ 

5. Compute the change in extinction coefficients:

in terms of deciviews:

$$dv = 10 \ln (1 + b_{exts}/b_{extb})$$

in terms of percent change of visibility:

$$\Delta\% = (b_{\text{exts}} / b_{\text{extb}}) \times 100$$

Based on the predicted SO₄, NO₃, and PM₁₀ concentrations, the proposed project's emissions will be compared to a 5 percent change in light extinction of the background levels. This is equivalent to a change in deciview of 0.5.

#### 3.2 Deposition Analyses

Deposition analyses will be performed for ENP for both total sulfur and total nitrogen. The analyses will follow those procedures and methodologies set forth in the IWAQM Phase II Report and the *Guide for Applying the USEPA Class I Screening Methodology with the CALPUFF Modeling System* document, developed by Earth Tech, Inc. (the model developers) in September 2001. This document is a guide for using the POSTUTIL processor to perform deposition analyses. Specifically, deposition analyses will be performed as follows:

- 1. Perform CALPUFF model runs using the specified options previously mentioned in Section 2.0 (including output of both dry and wet deposition).
- 2. Use POSTUTIL to combine the wet and dry flux output files from CALPUFF and scale the contributions of SO₂, SO₄, NO_x, NO₃, and HNO₃ such that total (i.e., wet and dry) nitrogen and total sulfur flux are contained in the same file. The POSTUTIL file is set up such that SO₂ and SO₄ contribute sulfur mass and SO₄, NO_x, HNO₃, and NO₃ contribute to the nitrogen mass.
- 3. Apply the appropriate scaling factors found in IWAQM Phase II Report (Section 3.3 Deposition Calculations) to the CALPOST runs to account for the conversion of grams to kilograms, square meters to hectares (ha), seconds to hours, and hours to a year. Thus, the CALPOST results are in kg/ha/yr.

The model-predicted results will be compared to the 0.01 kg/ha/year Deposition Analysis Threshold (DAT) developed jointly by the NPS and the U.S. Fish and Wildlife Service (FWS).

#### 3.3 Class I Impact Analysis

Ground-level impacts (in  $\mu g/m^3$ ) onto the ENP will be calculated for  $NO_x$ ,  $SO_2$ , and  $PM_{10}$  criteria pollutants for each applicable averaging period. The results of this analysis will be compared with the Class I Significant Impact Levels (SILs) calculated as 4 percent of the Class I Increment values. Should the model predicted impacts onto the ENP exceed the Class I SILs, an appropriately derived inventory of PSD increment consuming sources will be developed through FDEP and modeled with the CALPUFF modeling system for comparison to the Class I Increment values.

From: O'Neal, Brian D.

Sent: Monday, December 20, 2004 10:30 AM
To: Rinkol, Michael J.; Holmes, Allan R. (Bob)

Cc: Hillman, Timothy M. Subject: TCEC Modeling Protocol

Debbie Nelson (FDEP) got back to me today regarding some modeling issues/questions I left her with at the kick-off meeting last week.

She confirmed that the FDEP has no special modeling techniques when it comes to cooling towers; simply model as a point source.

She also confirmed that there are no Class II visibility areas near the project that we would need to model.

From: Nelson, Deborah [Deborah.Nelson@dep.state.fl.us]

Sent: Thursday, January 13, 2005 11:27 AM

To: O'Neal, Brian D.

Subject: Comments on Modeling Protocol for TCEC

Mr. O' Neal,

I will submit the Class I modeling protocol to the National Park Service for comments today. For the Class II, everything looked OK. Just make sure that you show how you determined the worst-case emission rates. For example, you stated in the protocol that for annual modeling impacts, the modeling will be based on annual average data at 100 percent load. Please show that the 100 percent load is a higher rate than 50 or 75% load. Please let me know if you have any questions and I will get back to you once I hear from the NPS.

Regards,

Debbie Nelson Meteorologist Air Permitting South 850-921-9537 deborah.nelson@dep.state.fl.us

From: Nelson, Deborah [Deborah.Nelson@dep.state.fl.us]

Sent: Tuesday, February 15, 2005 8:20 AM

To: O'Neal, Brian D.

Subject: RE: TCEC comments

Brian,

For the Met Data, 87-91 WPB is OK. If you want to use surface from Vero and Upper Air from WPB you may do so as well.

No word yet from the Park Service. It may take a while - weeks. If you are pressed for time you can address EPA's comments on the Class I modeling and submit an application. However, please know that the Park Service will still have comments coming which may require additional modeling.

Regards,

Debbie Nelson Meteorologist Air Permitting South 850-921-9537 deborah.nelson@dep.state.fl.us

----Original Message----

**From:** O'Neal, Brian D. [mailto:onealbd@bv.com] **Sent:** Monday, February 14, 2005 2:19 PM

To: Nelson, Deborah

Subject: RE: TCEC comments

Two questions:

- 1) Do you have any thoughts on the surface met data issue of West Palm Beach that EPA raised? This is very important as we are in the depths of the modeling analysis now.
- 2) Any word from the NPS on their comments?

Best Regards, Brian O'Neal

From: Nelson, Deborah [mailto:Deborah.Nelson@dep.state.fl.us]

Sent: Monday, February 07, 2005 2:09 PM

**To:** O'Neal, Brian D. **Subject:** TCEC comments

Brian.

EPA has given me comments. The NPS has informed me that they have comments as well. However, the NPS is not ready to give those to me yet. EPA's comments are as follows:

ISC-PRIME Model - A modification to the Class II area modeling protocol indicates ISC-PRIME is the proposed dispersion model. This is not an Appendix W regulatory model. Project specific approval is needed for the application of a non-regulatory model. Section 3.2.2 of the Guideline on Air Quality Models (40 CFR 51 Appendix W) provides the conditions



and documentation needed to obtain approval for the application of an alternated, non-guideline model. The reason ISCST3 is not appropriate for this application (Section 3.2.2.(b)) should be demonstrated and the basis for the acceptance of ISC-PRIME (section 3.2.2.(e)) should be provided.

You may send me your basis for using Prime and I can then forward it along to EPA if you'd like.

The TCEC appears to be located in the Midway Industrial Park. The fence line for TCEC should be the fence that is about the TCEC facility not that about the total industrial park (i.e., the fence line about the land owned or controlled by Florida Municipal power Agency).

- In addition to the maximum modeled concentrations, all concentrations challenging the maximum values (e.g., within 10 % of the maximum modeled concentration) should be modeled with a refined 100-m resolution grid.

The West Palm Beach meteorological data should be evaluated relative to other stations that may be more representative of the project locations (e. g., Vero Beach).

- A more recent 5-year period of record should be considered. The period of 1986-91 is more than a decade old. I will look more into this one and get back to you.

The pollutants to be modeled depends on the estimated emissions rates. All pollutant with significant emission rates should be modeled.

If emitted in sufficient amounts, PM2.5 and VOC (ozone) should be included in the PSD impact assessment

The 2.5 and VOC assessment should be a qualitative one.

Only emissions from the combined cycle combustion turbine are included in the protocol. Emissions from other facility components should be addressed.

- Emission values to be modeled should be associated with the maximum impacts not necessarily the maximum emission levels.

The components of the Additional Analysis portion of the required PSD impact analysis should be addressed. This includes impacts associated with growth, impacts on soils and vegetation, and visibility impacts to sensitive receptors within the impact area.

- The ambient air quality monitoring requirement should be addressed.

Class I Comments from EPA

FLM Review - The FLM for both Everglades NP and Chassahowitzka should be provided an opportunity to comment on the proposed modeling protocol.

- 2) Chassahowitzka Analysis Because Chasshowitzka appears to be about the same distance from the proposed project, this Class I area should be included in the analysis.
- 3) CALMET Settings When available, the horizontal and vertical CALMET grid settings should be provided. These should take into consideration the NWS data selected for inclusion in the modeling.
- 4) No Observations Option
  - Given a refined CALPUFF analysis appears to have been selected, the CALPUFF no observations option is not an regulatory application of this model. Appendix W Section 9.3.1.2.d addresses this issue. NWS observations in the modeling domain should be included.
- 5) Project Emissions The short-term and annual emission rates used in the Class II impact assessment should be used for this analysis. These should be the rates that produce the maximum impacts.



6) Additional Consultation - The protocol does not address the methods and procedure to be used if the extinction, deposition, and/or PSD increment assessments exceed their target values. If modeled values exceed the targets, the protocol should include further consultation with the regulatory agency with the possible need for a revised modeling protocol.

Let me know if you have any questions concerning these comments from EPA.

Debbie Nelson Meteorologist Air Permitting South 850-921-9537 deborah.nelson@dep.state.fl.us

From: Nelson, Deborah [Deborah.Nelson@dep.state.fl.us]

Sent: Tuesday, February 22, 2005 8:14 AM

To: O'Neal, Brian D.

Subject: RE: 138859.32.1100 050218 Responses to EPA Comments on Modeling Protocol

I received comments from the EPA regarding your responses to their comments on the modeling protocol. They agree that all of your responses are appropriate.

Debbie Nelson Meteorologist Air Permitting South 850-921-9537 deborah.nelson@dep.state.fl.us

----Original Message----

From: O'Neal, Brian D. [mailto:onealbd@bv.com]

Sent: Friday, February 18, 2005 3:46 PM

To: Nelson, Deborah

**Cc:** Kevin.Fleming@fmpa.com; SCHUMANN, SUSAN @ FMPA; AngelaM@hgslaw.com; Jody.Lamar.Finklea@fmpa.com; Fred.Bryant@fmpa.com; Armbruster, Stanley A. (Stan); Rollins, Myron R.; Soltys, J. Michael (Mike); Hillman, Timothy M.;

Holmes, Allan R. (Bob); TCEC; FortPierce@fmpa.com

Subject: 138859.32.1100 050218 Responses to EPA Comments on Modeling Protocol

Debbie.

Please find below our responses to the EPA comments on the Class I and Class II air dispersion modeling protocol for the Treasure Coast Energy Center. Let me know if you have any questions or concerns.

Best Regards, Brian O'Neal

From: Nelson, Deborah [mailto:Deborah.Nelson@dep.state.fl.us]

Sent: Monday, February 07, 2005 2:09 PM

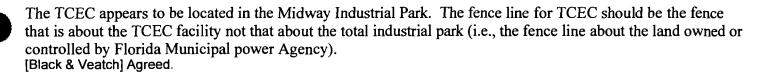
**To:** O'Neal, Brian D. **Subject:** TCEC comments

Brian,

EPA has given me comments. The NPS has informed me that they have comments as well. However, the NPS is not ready to give those to me yet. EPA's comments are as follows:

ISC-PRIME Model - A modification to the Class II area modeling protocol indicates ISC-PRIME is the proposed dispersion model. This is not an Appendix W regulatory model. Project specific approval is needed for the application of a non-regulatory model. Section 3.2.2 of the Guideline on Air Quality Models (40 CFR 51 Appendix W) provides the conditions and documentation needed to obtain approval for the application of an alternated, non-guideline model. The reason ISCST3 is not appropriate for this application (Section 3.2.2.(b)) should be demonstrated and the basis for the acceptance of ISC-PRIME (section 3.2.2.(e)) should be provided.

You may send me your basis for using Prime and I can then forward it along to EPA if you'd like. [Black & Veatch] That won't be necessary. The ISC-PRIME air dispersion model was simply inquired about as to its availability for usage in the state of Florida and was not necessarily proposed as the preferred air dispersion model for the project. We do not wish to pursue approval of ISC-PRIME at this point.



- In addition to the maximum modeled concentrations, all concentrations challenging the maximum values (e.g., within 10 % of the maximum modeled concentration) should be modeled with a refined 100-m resolution grid. [Black & Veatch] The project will comply with the request and the following protocol language is proposed: "If any maximum impact or controlling impact (i.e., a concentration within 10 percent of the maximum impact) occurs beyond the 100 m fine grid, a 100 m refined receptor grid surrounding the impact receptor out to a distance equal to the mid-point to the next receptor location in each direction will be placed around the impact to ensure that an absolute maximum concentration will be obtained from the model."

The West Palm Beach meteorological data should be evaluated relative to other stations that may be more representative of the project locations (e. g., Vero Beach).

- A more recent 5-year period of record should be considered. The period of 1986-91 is more than a decade old. I will look more into this one and get back to you.

[Black & Veatch] I realize you are looking into this Debbie. However, allow me to offer the following rationale for selecting West Palm Beach 1987 to 1991 data. The EPA's SCRAM website does not contain the required consecutive 5-year data set for Vero Beach. Also, 1987 to 1991 is the latest data set common to both the upper air and surface data stations available on the SCRAM website. Please let us know as soon as possible how to proceed on this issue.

The pollutants to be modeled depends on the estimated emissions rates. All pollutant with significant emission rates should be modeled.

If emitted in sufficient amounts, PM2.5 and VOC (ozone) should be included in the PSD impact assessment

The 2.5 and VOC assessment should be a qualitative one.

[Black & Veatch] Agreed. The extent of our analysis will be to provide our emissions estimates and PTE calculations of these pollutants.

Only emissions from the combined cycle combustion turbine are included in the protocol. Emissions from other facility components should be addressed.

- Emission values to be modeled should be associated with the maximum impacts not necessarily the maximum emission levels.

[Black & Veatch] Agreed. Emissions from other operating equipment such as the auxiliary boiler, fire pump, shutdown generator, and the cooling tower will be addressed (including emissions estimates, PTE calculations, and air dispersion modeling) in the air permit application document.

The components of the Additional Analysis portion of the required PSD impact analysis should be addressed. This includes impacts associated with growth, impacts on soils and vegetation, and visibility impacts to sensitive receptors within the impact area.

[Black & Veatch] Agreed. The Additional Impact Analysis will be addressed in the air permit application document.

- The ambient air quality monitoring requirement should be addressed.
[Black & Veatch] Agreed. The ambient air quality monitoring requirement will be addressed in the air permit application document. Furthermore, it is anticipated that the model-predicted, ground-level impacts from the proposed project will be below the de minimus ambient monitoring thresholds.

Class I Comments from EPA

1) FLM Review - The FLM for both Everglades NP and Chassahowitzka should be provided an opportunity to comment on the proposed modeling protocol.

[Black & Veatch] We assume FDEP has this for action.

- 2) Chassahowitzka Analysis Because Chasshowitzka appears to be about the same distance from the proposed project, this Class I area should be included in the analysis.

  [Black & Veatch] While Chassahowitzka is approximately 260 km away from the proposed project (a single Combined Cycle Combustion Turbine fired primarily on natural gas with limited ultra low sulfur fuel oil firing capabilities), the modeling domain will be extended to incorporate the proposed project's effects upon Chassahowitzka.
- 3) CALMET Settings When available, the horizontal and vertical CALMET grid settings should be provided. These should take into consideration the NWS data selected for inclusion in the modeling. [Black & Veatch] The horizontal grid settings are provided in the modeling protocol. The vertical grid settings were not as they vary with height, but generally are more tightly spaced near the surface and ultimately capped at 3,000 meters. The vertical grid settings are as follows: 0, 20, 40, 80, 160, 300, 600, 1,000, 1,500, 2,200, 3,000 meters.
- 4) No Observations Option
  - Given a refined CALPUFF analysis appears to have been selected, the CALPUFF no observations option is not an regulatory application of this model. Appendix W Section 9.3.1.2.d addresses this issue. NWS observations in the modeling domain should be included.

[Black & Veatch] With the No Observations Option being unacceptable, at our discretion, the Class I area air dispersion modeling analysis will consist of either a screening level analysis following the procedures set forth in EPA's Interagency Workgroup on Air quality Modeling (IWAQM) Phase 2 Summary Report and Recommendations for Modeling Long Range Transport Impacts (December 1998), Earth Tech, Inc.'s Guide for Applying the EPA Class I Screening Methodology with the CALPUFF Modeling System (September 2001), and the Long-Range-Transport Screening Technique Using CALPUFF document jointly authored by the National Park Service and the EPA or a full refined analysis that will include actual hourly data from surface, upper air, and precipitation stations within and around the new larger domain encompassing Chassahowitzka. Debbie, please be sure to communicate this updated methodology to the NPS.

- 5) Project Emissions The short-term and annual emission rates used in the Class II impact assessment should be used for this analysis. These should be the rates that produce the maximum impacts.

  [Black & Veatch] The maximum short-term emission rates will be used in the Class I modeling for all analyses.
- 6) Additional Consultation The protocol does not address the methods and procedure to be used if the extinction, deposition, and/or PSD increment assessments exceed their target values. If modeled values exceed the targets, the protocol should include further consultation with the regulatory agency with the possible need for a revised modeling protocol.

Black & Veatch] It is not expected that the proposed project will exceed any of the aforementioned target values. However, should the need arise, a cumulative source modeling methodology will be developed and presented to the FDEP for approval.

Let me know if you have any questions concerning these comments from EPA.

Debbie Nelson Meteorologist Air Permitting South 850-921-9537 deborah.nelson@dep.state.fl.us

From: O'Neal, Brian D.

Sent: Thursday, March 03, 2005 5:56 PM

To: Nelson, Deborah

Cc: SCHUMANN, SUSAN @ FMPA; AngelaM@hgslaw.com; Jody.Lamar.Finklea@fmpa.com;

Fred Bryant@fmpa.com; Armbruster, Stanley A. (Stan); Rollins, Myron R.; Soltys, J. Michael

(Mike); Hillman, Timothy M.; Holmes, Allan R. (Bob); TCEC; FortPierce@fmpa.com

Subject: RE: National Park Service Review of Treasure Coast Energy Modeling Protocol

#### Debbie.

Please find our response to the National Park Service's comments on our Class I air dispersion modeling protocol.

Based on the comments received from EPA Region IV, the proposed project's modeling domain has been extended to encompass both the Everglades National Park and the Chassahowitzka Wilderness Area. Given the new larger domain size requested by the EPA and the NPS Comment #2 below (to increase the grid resolution from 5 km to 3 km), a refined CALPUFF analysis becomes computer resource-intensive in nature and makes the CALMET output data files onerous to work with, store, and submit to the reviewing agency. In light of these considerations, it may be advantageous for the proposed project to choose the CALPUFF-Lite screening option.

The following are the modeling assumptions that will be invoked should the proposed project choose to perform CALPUFF-Lite screening modeling:

- 1) The Screening level analysis will follow the procedures set forth in the National Park Service's <u>Federal Land Managers'</u> <u>Air Quality Related Values Workgroup (FLAG) Phase I Report</u> (December 2000), Earth Tech, Inc.'s <u>Guide for Applying the EPA Class I Screening Methodology with the CALPUFF Modeling System</u> (September 2001), and the <u>Long-Range-Transport Screening Technique Using CALPUFF</u> document jointly authored by the National Park Service and the EPA.
- 2) Five years of National Weather Service data will be processed with CPRammet for use in the CALPUFF modeling. The data set will be 1987 through 1991 with surface data and upper air mixing height data from West Palm Beach, Florida. This is the same data set that was approved for use in the Class II air dispersion modeling demonstration. CPRammet is a modified version of the EPA meteorological processor PCRammet. It was created by Earth Tech, the developers of the CALPUFF modeling system. CPRammet was designed to alleviate two incompatibilities between PCRammet and the CALPUFF model: 1) PCRammet will not produce the necessary extended ISCST3 variables (e.g., friction velocity, Monin-Obukhov length, relative humidity, solar radiation, etc.) when input data are in CD-144 format and 2) PCRammet will not report solar radiation when an observed value is missing.

The data will be processed with CPRammet for wet deposition to produce the necessary extended ISCST3 variables. Values for surface roughness, albedo, Bowen ratio (average moisture), Monin-Obukhov length, and net radiation absorbed at the ground were derived from the June 1999 PCRammet User's Guide. For values where the specific land use type is required (i.e., surface roughness, albedo, and average moisture Bowen ratio), the Grassland land use category will be chosen and averaged over the 4 seasonal values provided to arrive at a single annual value for input into CPRammet. For the Monin-Obukhov length the Open Agricultural land use type and subsequent 2 meter value will be used. For the net radiation absorption value the rural value of 0.15 will be chosen. As indicated in the user's guide, anthropogenic heat flux will be assumed to be zero for areas outside highly urbanized locations. All 5 years of CPRammet processed data will be combined into a single 5-year meteorological data file.

- 3) Grid Settings: Since the screening methodology uses meteorological data from a single ISC meteorological data file, there is no spatial variation in meteorological or geophysical properties. Therefore, the minimum grid cell configuration of 2 grid cells in the x-direction and 2 grid cells in the y-direction will be used (4 grid cells total). A single layer will be used in the vertical since wind speed measurements taken at anemometer height will be scaled to stack-top height as in ISC. Therefore, the two cell face heights will be set to 0 meters (ground-level) and 5,000 meters (selected such that highest mixing height in the meteorological file does not exceed this value). The size of the domain will be of sufficient size to encompass the proposed project location, the Everglades National Park, and Chassahowitzka Wilderness Area with at least a 50 km buffer zone in each of the north, south, east, and west directions to allow for puffs to return to a Class I area due to a recirculating wind pattern.
- 4) The Mesopuff II chemical transformation methodology will be used with constant, default background values of ozone and ammonia (80 ppb and 10 ppb respectively).
- 5) Dry gas, dry particle, and wet deposition will be invoked.
- 6) The wind profile will be set to the ISC Rural setting with the calm wind speed set to 1.0 meters per second.

- 7) The only plume rise options that will be selected is Stacktip Downwash to simulate how a plume is handled in the ISC model.
- 8) The default Pasquill-Gifford coefficient with Rural ISC Curves will be selected for the dispersion option.
- 9) Terrain will be treated with the default Partial Plume Path Adjustment selection.
- 10) Emissions of NOx, SO2, PM10 (filterable and condensable), and SO4 will be input to the model. Furthermore, as requested, emissions of PM10 will be speciated based on size and composition. The recommendations on speciated particulate matter emissions estimates for natural gas and distillate oil fired turbines mentioned in the NPS comments below were requested from Don Shepherd as recommended. At this time, no response has been received. The proposed project will estimate the fraction of PM10 emissions that can be classified as filterable inorganic, filterable carbon, and condensable organic and will determine the various size categories for each composition. These speciated PM10 emissions will be classified into EC, SOA/OC, FPM (particles with mass mean diameters less than or equal to 2.5 microns), and CPM (particles with mass mean diameters greater than 2.5 microns but less than or equal to 10 microns).
- 11) Receptor rings will be created that pass through each Class I area. The receptor rings will have receptors spaced every 1 degree (i.e., 360 receptors per ring) with the proposed project's source located at the center of the ring. Each ring of receptors will have a single elevation. The elevation of the receptors in each ring will be set to the highest elevation found in the National Park Service-provided receptor database for each Class I area. The Everglades National Park will have 3 receptor rings passing through the area: one each at the nearest, mid-point, and most distant points of the area. Due to its small size, the Chassahowitzka Wilderness Area will have two receptor rings passing through the area: one each at the nearest and most distant points of the area. The highest impact occurring anywhere on the receptor rings for each Class I area will be reported as the maximum AQRV impact values for the proposed project. If necessary, the maximum impacts will be reported from the 90-degree and/or 45-degree arc of receptors on each side of the Class I area as indicated in the EPA/NPS Long-Range-Transport Screening Technique Using CALPUFF document.
- 12) The POSTUTIL processor will be used as described in the original Class I area air dispersion modeling protocol to determine the impacts of total sulfur and total nitrogen deposition in kg/ha/yr upon each Class I area.

The POSTUTIL processor will also be used to group the size-speciated particulate emissions into the appropriate compositions of EC, SOA/OC, FPM, CPM, and PM10 emissions by multiplying the nominal 1 gram per second emission rates in CALPUFF by the appropriate speciated PM10 emissions (based on size and composition).

13) Visibility will be computed by using the model-predicted components of NO3, SO4, OC/SOA, PMC, PMF, and EC. Visibility calculations will be performed as recommended in the FLAG document by using Method 6 and the Class I areaspecific seasonal values of Hygroscopic, Non-Hygroscopic, Rayleigh, and Relative Humidity Factors given the in the document.

Regards, Brian O'Neal

From:

Nelson, Deborah [mailto:Deborah.Nelson@dep.state.fl.us]

Sent:

Monday, February 28, 2005 11:21 AM

To:

O'Neal, Brian D.

Subject:

FW: National Park Service Review of Treasure Coast Energy Modeling Protocol

Comments from the Park Service...

Debbie Nelson Meteorologist Air Permitting South 850-921-9537 deborah.nelson@dep.state.fl.us

——Original Message-----

From: Dee_Morse@nps.gov [mailto:Dee_Morse@nps.gov]

Sent: Monday, February 28, 2005 11:32 AM

To: Nelson, Deborah

Cc: John_Bunyak@nps.gov; John_Notar@nps.gov; Don_Shepherd@nps.gov; HGebhart@air-resource.com

#### Debbie.

We have the following comments regarding the CALPUFF dispersion modeling protocol for the Treasure Coast Energy Center Combined Cycle Unit 1 prepared by Black and Veatch dated January 2005.

- 1. We agree with comments provided by Environmental Protection Agency (EPA) Region IV that the "no observation" mode of CALPUFF should not be employed. Our understanding from Black and Veatch's response to EPA's comments is that they will employ either a CALPUFF-Lite screening modeling approach, or a refined CALPUFF modeling analysis using appropriate National Weather Service (NWS) surface, upper air, and precipitation stations from the modeling domain. Either approach would be acceptable. However, the protocol lacks specific information about the CALPUFF-Lite screening option.
- 2. The applicant's proposed grid size for CALPUFF is 5 km, presuming that a refined modeling analysis is conducted. We would prefer that a smaller grid size be used. A 3-km horizontal grid spacing would be acceptable and would also define the nearby coastline (which can be important for plume dispersion) with greater resolution.
- 3. The modeling domain for this study includes both overland and overwater grid cells. Some NWS surface stations that might be employed in the meteorological data field development for the refined CALPUFF modeling are located along the coastline where they are subjected to the land breeze/sea breeze phenomena. We would caution the applicant to select appropriate "radius of influence" parameters so that the land breeze/sea breeze effects present in the NWS data do not extend too far inland or offshore.
- 4. Based on the response to EPA comments, the applicant is committing to model the maximum short-term emission rates, but the specific emissions were not listed. The protocol indicates that only emissions of nitrogen oxides (NOx), sulfur dioxide (SO2) and particulate matter (PM-10) will be modeled. The applicant should be advised that the PM-10 emissions need to include the condensable fraction and should not be based only on the filterable PM-10 emissions. Also, consistent with other recent CALPUFF modeling, the applicant should model stack emissions for primary sulfate (SO4) as well as speciated PM-10 (EC, SOA, & FPM). We have developed recommendations on sulfate and speciated particulate matter emission estimates for natural gas-fired and distillate oil-fired turbines. Please contact Don Shepherd (National Park Service Air Resources Division don shepherd@nps.gov) for these emission estimates.
- 5. The applicant has proposed a background ammonia concentration of 0.5 ppb, which is from the IWAQM Phase II Report for "forested" areas. We do not believe that the proposed ammonia background data are representative of conditions in south Florida. Our understanding is that the land use along the likely trajectory to Everglades National Park consists primarily of agricultural lands, and undeveloped marshes/swamps. The immediate area surrounding the source is also urbanized to some degree. All of these lands would be expected to generate higher background ammonia levels than "forested" lands. As such, our recommendation is to use the 10 ppb background ammonia value listed by the IWAQM report for "grasslands" or at least computed a "weighted mean" based on the land use patterns actually present in the modeling domain.

Please contact me if there are any questions concerning our comments.

Thanks,

Dee Morse Environmental Protection Specialist National Park Service Air Resources Division (303) 969-2817 dee_morse@nps.gov



# Department of Environmental Protection

# Division of Air Resource Management APPLICATION FOR AIR PERMIT - LONG FORM

#### I. APPLICATION INFORMATION

Air Construction Permit – Use this form to apply for an air construction permit for a proposed project:

- subject to prevention of significant deterioration (PSD) review, nonattainment area (NAA) new source review, or maximum achievable control technology (MACT) review; or
- where the applicant proposes to assume a restriction on the potential emissions of one or more pollutants to escape a federal program requirement such as PSD review, NAA new source review, Title V, or MACT; or
- at an existing federally enforceable state air operation permit (FESOP) or Title V permitted facility.

#### Air Operation Permit - Use this form to apply for:

- an initial federally enforceable state air operation permit (FESOP); or
- an initial/revised/renewal Title V air operation permit.

Air Construction Permit & Revised/Renewal Title V Air Operation Permit (Concurrent Processing Option)

- Use this form to apply for both an air construction permit and a revised or renewal Title V air operation permit incorporating the proposed project.

To ensure accuracy, please see form instructions.

#### **Identification of Facility**

1.	Facility Owner/Company Name: Florida Municipal Power Agency				
2.	Site Name: Treasure Coast Energy Center				
3.	Facility Identification Number:				
4.	Facility Location				
	Street Address or Other Locator: 4585 Sel-	vitz Road, Lot 8			
	City: Fort Pierce County: S	St. Lucie Zip Code:			
5.	Relocatable Facility?	6. Existing Title V Permitted Facility?			
	Yes X No	Yes x No			
Ar	oplication Contact	-			
1.	Application Contact Name: Susan Schuma	ann			
2.	2. Application Contact Mailing Address				
	Organization/Firm: Florida Municipal Power Agency				
	Street Address: 8553 Commodity Circle				
	City: Orlando Si	tate: FL Zip Code: 32819			
3.	Application Contact Telephone Numbers				
	Telephone: (407) 355-7767 ext.	Fax: (407) 355-5794			
4.	4. Application Contact Email Address: susan.schumann@fmpa.com				
<u>Ar</u>	Application Processing Information (DEP Use)				
1.	Date of Receipt of Application:	4-14-05			
2.	Project Number(s):	1110121-001-AC			
3.	PSD Number (if applicable):	1110121-001-AC PSO-FL-353			
4.	Siting Number (if applicable):				

DEP Form No. 62-210.900(1) – Form Effective: 06/16/03

#### **Purpose of Application**

This application for air permit is submitted to obtain: (Check one) **Air Construction Permit** X Air construction permit. **Air Operation Permit** Initial Title V air operation permit. Title V air operation permit revision. Title V air operation permit renewal. Initial federally enforceable state air operation permit (FESOP) where professional engineer (PE) certification is required. Initial federally enforceable state air operation permit (FESOP) where professional engineer (PE) certification is not required. Air Construction Permit and Revised/Renewal Title V Air Operation Permit (Concurrent Processing) Air construction permit and Title V permit revision, incorporating the proposed project. Air construction permit and Title V permit renewal, incorporating the proposed project. Note: By checking one of the above two boxes, you, the applicant, are requesting concurrent processing pursuant to Rule 62-213.405, F.A.C. In such case, you must also check the following box: I hereby request that the department waive the processing time requirements of the air construction permit to accommodate the processing time frames of the Title V air operation permit. Application Comment

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Effective: 06/16/03

## **Scope of Application**

Emissions	Description of Francis - Half	Air	Air
Unit ID Number	Description of Emissions Unit	Permit Type	Permit Proc. Fee
	Unit 1 – GE PG7241 FA Combustion Turbine	AC1A	NA
	Auxiliary Boiler	AC1A	NA
	Diesel Engine Fire Pump	AC1A	NA
	Safe Shutdown Generator	AC1A	NA
	Fuel Oil Storage Tank – 990,000 gallon fuel oil storage tank	AC1F	NA
	Mechanical Draft Cooling Tower	AC1A	NA
		·	

Application Processing Fee	
Check one: Attached - Amount: \$	X Not Applicable

Effective: 06/16/03 3

#### Owner/Authorized Representative Statement

Complete if applying for an air construction permit or an initial FESOP.

- Owner/Authorized Representative Name : Roger Fontes – General Manager and CEO
- 2. Owner/Authorized Representative Mailing Address... Organization/Firm: Florida Municipal Power Agency

Street Address: 8553 Commodity Circle

City: Orlando

State: FL

Zip Code: 32819

- 3. Owner/Authorized Representative Telephone Numbers...
  Telephone: (407) 355-7767 ext. Fax: (407) 355-5794
- 4. Owner/Authorized Representative Email Address: roger.fontes@fmpa.com
- 5. Owner/Authorized Representative Statement:

I, the undersigned, am the owner or authorized representative of the facility addressed in this air permit application. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements made in this application are true, accurate and complete and that, to the best of my knowledge, any estimates of emissions reported in this application are based upon reasonable techniques for calculating emissions. The air pollutant emissions units and air pollution control equipment described in this application will be operated and maintained so as to comply with all applicable standards for control of air pollutant emissions found in the statutes of the State of Florida and rules of the Department of Environmental Protection and revisions thereof and all other requirements identified in this application to which the facility is subject. I understand that a permit, if granted by the department, cannot be transferred without authorization from the department, and I will promptly notify the department upon sale or legal transfer of the facility or any permitted emissions unit.

Signature

Date

4/11/05

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## **Application Responsible Official Certification**

Complete if applying for an initial/revised/renewal Title V permit or concurrent processing of an air construction permit and a revised/renewal Title V permit. If there are multiple responsible officials, the "application responsible official" need not be the "primary responsible official."

1.	Application Responsible Official Name:
2.	Application Responsible Official Qualification (Check one or more of the following options, as applicable):
	For a corporation, the president, secretary, treasurer, or vice-president of the corporation in charge of a principal business function, or any other person who performs similar policy or decision-making functions for the corporation, or a duly authorized representative of such person if the representative is responsible for the overall operation of one or more manufacturing, production, or operating facilities applying for or subject to a permit under Chapter 62-213, F.A.C.
	For a partnership or sole proprietorship, a general partner or the proprietor, respectively.
	For a municipality, county, state, federal, or other public agency, either a principal executive officer or ranking elected official.
	The designated representative at an Acid Rain source.
3.	Application Responsible Official Mailing Address
	Organization/Firm:
	Street Address:
	City: State: Zip Code:
4.	Application Responsible Official Telephone Numbers
	Telephone: ( ) - ext. Fax: ( ) -
	Application Responsible Official Email Address:
6.	Application Responsible Official Certification:
	I, the undersigned, am a responsible official of the Title V source addressed in this air permit application. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements made in this application are true, accurate and complete and that, to the best of my knowledge, any estimates of emissions reported in this application are based upon reasonable techniques for calculating emissions. The air pollutant emissions units and air pollution control equipment described in this application will be operated and maintained so as to comply with all applicable standards for control of air pollutant emissions found in the statutes of the State of Florida and rules of the Department of Environmental Protection and revisions thereof and all other applicable requirements identified in this application to which the Title V source is subject. I understand that a permit, if granted by the department, cannot be transferred without authorization from the department, and I will promptly notify the department upon sale or legal transfer of the facility or any permitted emissions unit. Finally, I certify that the facility and each emissions unit are in compliance with all applicable requirements to which they are subject, except as identified in compliance plan(s) submitted with this application.
	Signature Date

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DEP Form No. 62-210.900(1) – Form

<u>Pr</u>	ofessional Engineer Certification
1.	Professional Engineer Name: Stanley A. Armbruster, P.E.
	Registration Number: 30562
2.	Professional Engineer Mailing Address
	Organization/Firm: Black & Veatch
	Street Address: 11401 Lamar Avenue
	City: Overland Park State: KS Zip Code: 66211
3.	Professional Engineer Telephone Numbers
	Telephone: (913) 458-2763 ext. Fax: (913) 458-2934
4.	Professional Engineer Email Address: ArmbrusterSA@bv.com
5.	Professional Engineer Statement:
	I, the undersigned, hereby certify, except as particularly noted herein*, that:
	(1) To the best of my knowledge, there is reasonable assurance that the air pollutant emissions
	unit(s) and the air pollution control equipment described in this application for air permit, when
	properly operated and maintained, will comply with all applicable standards for control of air
	pollutant emissions found in the Florida Statutes and rules of the Department of Environmental Protection; and
	(2) To the best of my knowledge, any emission estimates reported or relied on in this application
	are true, accurate, and complete and are either based upon reasonable techniques available for
	calculating emissions or, for emission estimates of hazardous air pollutants not regulated for an
	emissions unit addressed in this application, based solely upon the materials, information and
	calculations submitted with this application.
	(3) If the purpose of this application is to obtain a Title V air operation permit (check here, if
	so), I further certify that each emissions unit described in this application for air permit, when properly operated and maintained, will comply with the applicable requirements identified in this
	application to which the unit is subject, except those emissions units for which a compliance plan
	and schedule is submitted with this application.
	(4) If the purpose of this application is to obtain an air construction permit (check here $x$ , if so)
	or concurrently process and obtain an air construction permit and a Title V air operation permit
	revision or renewal for one or more proposed new or modified emissions units (check here, if
	so), I further certify that the engineering features of each such emissions unit described in this
	application have been designed or examined by me or individuals under my direct supervision and found to be in conformity with sound engineering principles applicable to the control of emissions
Ì	of the air pollutants characterized in this application.
	(5) If the purpose of this application is to obtain an initial air operation permit or operation
	permit revision or renewal for one or more newly constructed or modified emissions units (check
	here [ ], if so), I further certify that, with the exception of any changes detailed as part of this
	application, each such emissions unit has been constructed or modified in substantial accordance with the information given in the corresponding application for air construction permit and with
ĺ	all provisions contained in such permit.
	ARMONIUM
	Signal Standard April 14 2005
	Signarius Date
	(seat) +
L	(John )

Attached exception to certification statement

DEP Form No. 2-210-900 A Torm Effective: 06/46/63 NA

#### II. FACILITY INFORMATION

#### A. GENERAL FACILITY INFORMATION

## Facility Location and Type

1.	1. Facility UTM Coordinates  Zone 17 East (km) 561.5161  North (km) 3028.9963			2. Facility Latitude/Longitude Latitude (DD/MM/SS) Longitude (DD/MM/SS)		
3.	3. Governmental 4. Facility Status Code: 4 C		5.	Facility Major Group SIC Code: 4911 49		
7.	Facility Comment:					

## **Facility Contact**

1.	Facility Contact Name Jim Hay			
2.	Facility Contact Mailing Addres	S		
	Organization/Firm: Florida Mur	nicipal Power Agency	1	
	Street Address: 8553 Comm	odity Circle		
	City: Orlando	State: FL	Zip Code: 32819	
3.	Facility Contact Telephone Num	bers:		
	Telephone: (407) 355-7767	ext.	Fax: (407) 355-5794	
4.	Facility Contact Email Address:	jim.hay@fmpa.com		

## Facility Primary Responsible Official

Complete if an "application responsible official" is identified in Section I. that is not the facility "primary responsible official."

	<u> </u>					
l.	Facility Primary Responsi	ble Officia	ıl Name:			
2.	Facility Primary Responsible Organization/Firm: Street Address:	ble Officia	ll Mailing Ad	dress		
	City:		State:		Zip Code:	
3.	Facility Primary Responsil	ble Officia	l Telephone	Numbers		
	Telephone: ( ) -	ext.	Fax: ( ) -			
4.	Facility Primary Responsi	ble Officia	ıl Email Addr	ess:		

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#### **FACILITY INFORMATION**

## Facility Regulatory Classifications

Check all that would apply *following* completion of all projects and implementation of all other changes proposed in this application for air permit. Refer to instructions to distinguish between a "major source" and a "synthetic minor source."

1.  Small Business Stationary Source Unknown
2. Synthetic Non-Title V Source
3. x Title V Source
4. X Major Source of Air Pollutants, Other than Hazardous Air Pollutants (HAPs)
5. Synthetic Minor Source of Air Pollutants, Other than HAPs
6. Major Source of Hazardous Air Pollutants (HAPs)
7. Synthetic Minor Source of HAPs
8.   One or More Emissions Units Subject to NSPS (40 CFR Part 60)
9.  One or More Emissions Units Subject to Emission Guidelines (40 CFR Part 60)
10.  One or More Emissions Units Subject to NESHAP (40 CFR Part 61 or Part 63)
11. Title V Source Solely by EPA Designation (40 CFR 70.3(a)(5))
12. Facility Regulatory Classifications Comment:

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## **FACILITY INFORMATION**

## List of Pollutants Emitted by Facility

1. Pollutant Emitted	2. Pollutant Classification	3. Emissions Cap [Y or N]?	
СО	A	N.	
NOX	A	N	
PM	A	N	
PM10	A	N	
SO2	В	N	
VOC	В	N	
SAM	В	N	
	·		

## **FACILITY INFORMATION**

## **B. EMISSIONS CAPS**

## Facility-Wide or Multi-Unit Emissions Caps

1. Pollutant Subject to Emissions Cap	2. Facility Wide Cap [Y or N]? (all units)	3. Emissions Unit ID No.s Under Cap (if not all units)	4. Hourly Cap (lb/hr)	5. Annual Cap (ton/yr)	6. Basis for Emissions Cap
		_			
		-			

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7. Facility-Wide or Multi-Unit Emissions Cap Comment:

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## C. FACILITY ADDITIONAL INFORMATION

## Additional Requirements for All Applications, Except as Otherwise Stated

1. Facility Plot Plan: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within t previous five years and would not be altered as a result of the revision being sought)	he			
x Attached, Document ID: Attach. A Previously Submitted, Date:				
2. Process Flow Diagram(s): (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the departme within the previous five years and would not be altered as a result of the revision being sought)  X Attached, Document ID: Attach. B Previously Submitted, Date:	nt			
3. Precautions to Prevent Emissions of Unconfined Particulate Matter: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  X Attached, Document ID: Attach. C Previously Submitted, Date:	ot			
Additional Dequipments for Air Construction Descrit Applications				
Additional Requirements for Air Construction Permit Applications				
Area Map Showing Facility Location:      X Attached, Document ID: Attach. D       Not Applicable (existing permitted facility states)    X	y)			
Description of Proposed Construction or Modification:     X Attached, Document ID: Attach. E				
3. Rule Applicability Analysis:  x Attached, Document ID: Attach. F				
4. List of Exempt Emissions Units (Rule 62-210.300(3)(a) or (b)1., F.A.C.):	.y)			
5. Fugitive Emissions Identification (Rule 62-212.400(2), F.A.C.):  Attached, Document ID: x Not Applicable				
6. Preconstruction Air Quality Monitoring and Analysis (Rule 62-212.400(5)(f), F.A.C.):				
7. Ambient Impact Analysis (Rule 62-212.400(5)(d), F.A.C.):				
8. Air Quality Impact since 1977 (Rule 62-212.400(5)(h)5., F.A.C.):				
9. Additional Impact Analyses (Rules 62-212.400(5)(e)1. and 62-212.500(4)(e), F.A.C.):				
10. Alternative Analysis Requirement (Rule 62-212.500(4)(g), F.A.C.):  Attached, Document ID: x Not Applicable				

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### **FACILITY INFORMATION**

### **Additional Requirements for FESOP Applications**

1.	List of Exempt Emissions Units (Rule 62-210.300(3)(a) or (b)1., F.A.C.):					
	Attached, Document ID: Not Applicable (no exempt units at facility)					
A	Additional Requirements for Title V Air Operation Permit Applications					
1.	List of Insignificant Activities (Required for initial/renewal applications only):  Attached, Document ID: Not Applicable (revision application)					
2.	Identification of Applicable Requirements (Required for initial/renewal applications, and for revision applications if this information would be changed as a result of the revision being sought):  Attached, Document ID:  Not Applicable (revision application with no change in applicable requirements)					
3.	Compliance Report and Plan (Required for all initial/revision/renewal applications):  Attached, Document ID:  Note: A compliance plan must be submitted for each emissions unit that is not in compliance with all applicable requirements at the time of application and/or at any time during application processing. The department must be notified of any changes in compliance status during application processing.					
4.	List of Equipment/Activities Regulated under Title VI (If applicable, required for initial/renewal applications only):  Attached, Document ID:  Equipment/Activities On site but Not Required to be Individually Listed  Not Applicable					
5.						
	☐ Attached, Document ID: ☐ Not Applicable					
6.	Requested Changes to Current Title V Air Operation Permit:  Attached, Document ID: Not Applicable					
<u>A</u>	dditional Requirements Comment					
_	ttachment S includes a CD with air dispersion modeling files.					

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#### III. EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Application - For Title V air operation permitting only, emissions units are classified as regulated, unregulated, or insignificant. If this is an application for Title V air operation permit, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each regulated and unregulated emissions unit addressed in this application for air permit. Some of the subsections comprising the Emissions Unit Information Section of the form are optional for unregulated emissions units. Each such subsection is appropriately marked. Insignificant emissions units are required to be listed at Section II, Subsection C.

Air Construction Permit or FESOP Application - For air construction permitting or federally enforceable state air operation permitting, emissions units are classified as either subject to air permitting or exempt from air permitting. The concept of an "unregulated emissions unit" does not apply. If this is an application for air construction permit or FESOP, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air permitting are required to be listed at Section II, Subsection C.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit Application — Where this application is used to apply for both an air construction permit and a revised/renewal Title V air operation permit, each emissions unit is classified as either subject to air permitting or exempt from air permitting for air construction permitting purposes and as regulated, unregulated, or insignificant for Title V air operation permitting purposes. The air construction permitting classification must be used to complete the Emissions Unit Information Section of this application for air permit. A separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air construction permitting and insignificant emissions units are required to be listed at Section II, Subsection C.

If submitting the application form in hard copy, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application must be indicated in the space provided at the top of each page.

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#### A. GENERAL EMISSIONS UNIT INFORMATION

### Title V Air Operation Permit Emissions Unit Classification

	1.	. Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)								
		<ul> <li>☐ The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.</li> <li>☐ The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.</li> </ul>								
	<u>Em</u>	nissions Unit	Description and Sta	ntus						
ſ	1.	Type of Emis	ssions Unit Addresse	d in this Sectio	n: (Check one)					
		single pro	ocess or production u	mit, or activity,	addresses, as a single which produces one of point (stack or vent)	or more air pollutants				
		process of		d activities wh	ich has at least one de	issions unit, a group of finable emission point				
1					lresses, as a single em es which produce fugi	-				
	2.	Description of Combustion		ldressed in this	Section: Unit 1 – GE	E PG7241 FA				
	3.	Emissions U	nit Identification Nu	mber:						
	4.	Emissions Unit Status Code: C	5. Commence Construction Date:	6. Initial Startup Date:	7. Emissions Unit Major Group SIC Code: 49	8. Acid Rain Unit?  x Yes  No				
	9.	Package Unit Manufacturer			Model Number: PG7	7241 FA				
ŀ	10.			70 MW for the	CT (approximate):	7241 I A				
			-		STG (approximate)					
	11.	Emissions Ur firing capabil		ombined cycle	combustion turbine w	vill include HRSG duct				
			•							

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### **Emissions Unit Control Equipment**

1.	Dry low NO _x burners in conjunction with selective catalytic reduction will be used to control NO _x emissions when firing natural gas.  Water injection in combination with selective catalytic reduction will be used to control NO _x emissions when firing fuel oil.								

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2. Control Device or Method Code(s): 205, 028, 139

#### **B. EMISSIONS UNIT CAPACITY INFORMATION**

(Optional for unregulated emissions units.)

#### Emissions Unit Operating Capacity and Schedule

1.	Maximum	Process of	Throughput Rate:
----	---------	------------	------------------

2. Maximum Production Rate:

3. Maximum Heat Input Rate: 1,876.8 million Btu/hr (HHV) - CT firing natural gas

2,044.4 million Btu/hr (HHV) – CT firing fuel oil

565.3 million Btu/hr (HHV) - Duct Burner

4. Maximum Incineration Rate: pounds/hr

tons/day

5. Requested Maximum Operating Schedule:

CT firing natural gas 24 hours/day 7 days/week

52 weeks/year 8,760 hours/year

Duct burner firing natural gas 24 hours/day 7 days/week

52 weeks/year 8,760 hours/year

CT firing fuel oil 24 hours/day 7 days/week

52 weeks/year 500 hours/year

6. Operating Capacity/Schedule Comment: The unit will be operated between 40 and 100 percent of full load. The maximum heat input rate shown in Field 3 is with operation at 100% load at the site minimum ambient temperature of 26°F. Note that the heat input rate is a function of ambient temperature. As discussed in FDEP Guidance Document DARM-OGG-07, higher CT inlet temperatures will result in a lower heat input rate (MMBtu/hr) and vice versa. Variations of heat input (capacity) are to be expected due to the range of ambient temperatures and humidities encountered at the site. When they become available, the CT operating curves (capacity vs. inlet air temperature) will be provided to the Department. It is requested that the permit for this unit include Conditions 1 and 2 of DARM-OGG-07. We request inclusion of the standard permitting note that the heat input rates are provided for informational purposes only and are not intended to be enforceable limits.

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# C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

### **Emission Point Description and Type**

1.	. Identification of Point on Plot Plan or		2. Emission Point Type Code:			
	Flow Diagram: Heat Recovery Steam		1			
	Generator Exhaust Stack					
3.	Descriptions of Emission	Points Comprising	g this Emissions Unit	for VE Tracking:		
4.	ID Numbers or Descriptio	ns of Emission Ur	nits with this Emissior	Point in Common:		
	-					
5	Discharge Type Code:	6. Stack Height		7. Exit Diameter:		
].	V	170 feet	•	18 feet		
R	Exit Temperature:		metric Flow Rate:	10. Water Vapor:		
0.	170°F	958,300 acfr		12%		
11.	Maximum Dry Standard F	low Rate:	12. Nonstack Emission Point Height:			
	793,000 dscfm		Territorio de la constantina della constantina d			
13.	Emission Point UTM Coo	rdinates	14. Emission Point Latitude/Longitude			
	Zone: 17 East (km):	561.5161	Latitude (DD/MM/SS)			
	North (km)	: 3028.9963	Longitude (DD/I	MM/SS)		
15.	Emission Point Comment	: Emission point i	nformation given in F	Fields 8 through 11 are		
	based on firing natural gas					
	temperature of 73°F and H					
	ambient temperature and 1		_	_		
	with operation at 100% los HRSG duct firing.	au and at the site a	iverage amolem temp	erature of 73°F and		
	Field 8: 250°F					
	Field 9: 1,135,600 acfm					
	Field 10: 15%					
	Field 11: 830,600 scfm					

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### **EMISSIONS UNIT INFORMATION**

Section [1]

of [6]

#### D. SEGMENT (PROCESS/FUEL) INFORMATION

### Segment Description and Rate: Segment 1 of 3

Segment Description (Proc Natural gas used in the con	·	<b>;</b>					
2. Source Classification Code 20100201	e (SCC):	3. SCC Units: Million Cub	oic Feet Burned				
4. Maximum Hourly Rate: 1.93	5. Maximum Annual Rate: 16,907		6. Estimated Annual Activity Factor:				
7. Maximum % Sulfur:	8. Maximum	% Ash:	9. Million Btu per SCC Unit: 970 (HHV)				
10. Segment Comment: The maximum fuel input to the combustion turbine is a function of the ambient temperature. The maximum hourly rate given in Field 4 is based on operation at 100% load at the site minimum ambient temperature of 26°F. The maximum natural gas use rate given in Field 5 is based on 100 percent load operation for 8,760 hours per year at the site minimum ambient temperature of 26°F. The fuel use rates do not include duct burner operation.							
Segment Description and Ra	te: Segment 2 o	of <u>3</u>					
Segment Description (Process/Fuel Type):     No. 2 fuel oil used in the combustion turbine							

2.	Source Classification Code 20100101	e (SCC):	3. SCC Units: Thousand gallons burned		
4.	Maximum Hourly Rate: 14.9	5. Maximum Annual Rate: 7,450		6. Estimated Annual Activity Factor:	
7.	Maximum % Sulfur: 0.0015	8. Maximum % Ash:		9. Million Btu per SCC Unit: 137 (HHV)	

10. Segment Comment: The maximum fuel input to the combustion turbine is a function of the ambient temperature. The maximum hourly rate given in Field 4 is based on operation at 100% load at the site minimum ambient temperature of 26°F. The maximum fuel oil use rate given in Field 5 is based on 100 percent load operation for 500 hours per year at the site minimum ambient temperature of 26°F.

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### D. SEGMENT (PROCESS/FUEL) INFORMATION (CONTINUED)

Segment Description and Rate: Segment 3 of 3

1.	Segment Description (Process/Fuel Type):							
	Natural gas used in duct burner.							
2.	Source Classification Code	e (SCC):	3. SCC Units:					
	<del></del>			bic Feet Burned				
4.	Maximum Hourly Rate:	5. Maximum	Annual Rate:	6. Estimated Annual Activity				
<u></u>	0.58	5,105		Factor:				
7.	Maximum % Sulfur:	8. Maximum	% Ash:	9. Million Btu per SCC Unit: 970 (HHV)				
10.	•			ural gas. The duct burner may				
	operate when firing either	natural gas or fu	el oil in the comb	bustion turbine.				
Sec	gment Description and Ra	ite: Segment	of					
	·							
1.	Segment Description (Prod	cess/ruel Type):						
2.	Source Classification Cod	· (SCC)·	3. SCC Units:	•				
2.	Source Classification Cou		3. See Onits:	•				
1	Maximum Hourly Rate:	5. Maximum	Annual Date:	6. Estimated Annual Activity				
4.	Maximum Houry Rate.	J. Waxiiiiuiii	Alliluai Kalt.	Factor:				
7	Maximum % Sulfur:	8. Maximum	% Ash·	9. Million Btu per SCC Unit:				
'`	Manimum / V Dunium.	o. Maximum	/ U I ADII.	J. Million Bu per See Offit.				
10	. Segment Comment:							
10.	. Deginem Comment.							

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### E. EMISSIONS UNIT POLLUTANTS

### List of Pollutants Emitted by Emissions Unit

1. Pollutant Emitted	Primary Control     Device Code	Secondary Control     Device Code	Pollutant     Regulatory Code
СО			
NOX	205, 139 (NG)		EL
	028, 139 (FO)		
PM			
PM10			
SO2			WP
voc			
SAM			WP

## POLLUTANT DETAIL INFORMATION [1] of [17]

# F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

applying for an arr operation permit.					
1.	Pollutant Emitted:	2. Total Percent Efficiency of Control:		ency of Control:	
	CO				
3.	Potential Emissions:		4. Synth	netically Limited?	
	92.4 lb/hour 228.	5 tons/year	х	Yes No	
5.	Range of Estimated Fugitive Emissions (as	applicable):			
	to tons/year				
6.	Emission Factor:			7. Emissions	
				Method Code:	
]	Reference: Vendor Data			5	
8.	Calculation of Emissions:				
	Potential emissions are based on vendor dat	a.			
	The maximum hourly potential CO emissio				
	mode firing fuel oil in the combustion turbi				
	burner and operation at an ambient tempera	ture of 26°F. T	he maxim	um hourly CO	
	emission rate is 92.4 lb/hour.				
	The maximum annual potential CO emissio				
	mode firing fuel oil in the combustion turbi	•			
	firing natural gas in the combustion turbine	-		•	
	and firing natural gas in the duct burner for	8,760 hours per	r year and	operation at the site	
	average ambient temperature of 73°F.	. 50 1 11-7	2601-7	) 1 +/2 000 II	
	Annual emissions = $(86.2 \text{ lb/hr x } 500 \text{ hr/yr})$	+ 50.1 lb/nr x 8	,200 nr/yr	) x 1 ton/2,000 lb =	
9.	228.5 tons/year Pollutant Potential/Estimated Fugitive Emis	ssions Common	+•		
٦.	The following are the maximum CO emissi			5 percent Oc.	
	Combined cycle natural gas firing: 10.4 pp		iv, uiy at 1	5 percent O2.	
	Combined cycle fuel oil firing: 15.4 ppmvo				
	Potential emission estimates are given for in		irnoses and	d do not represent	
	limits.	o.macionai pa	rposes and	a do not represent	
	*********				

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## POLLUTANT DETAIL INFORMATION Page [2] of [17]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions	_of			
Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:			
	lb/hour tons/year			
5. Method of Compliance:				
6. Allowable Emissions Comment (Descriptio	n of Operating Method):			
Allowable Emissions Allowable Emissions	_of			
Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year			
Method of Compliance:      Allowable Emissions Comment (Description)	on of Operating Method):			
Allowable Emissions Allowable Emissions	of			
Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:			
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year			
5. Method of Compliance:				
6. Allowable Emissions Comment (Description	on of Operating Method):			

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## POLLUTANT DETAIL INFORMATION Page [3] of [17]

# F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted: NOX	2. Total Perc	ent ]	Effici	ency of Control:	
3.	Potential Emissions:		4.	-	hetically Limited?	
		l tons/year		х	Yes No	
5.	5. Range of Estimated Fugitive Emissions (as applicable): to tons/year					
6.	Emission Factor:				7. Emissions	
]	Reference: Vendor Data				Method Code: 5	
8.	Calculation of Emissions:					
	Potential emissions are based on vendor dat					
	The maximum hourly potential NO _x emission combustion turbine at 100% load, firing nat			_		
	ambient temperature of 26°F. The maximum	_			-	
	The maximum annual potential NO _x emission	•				
	combustion turbine at 100 percent load for			_		
	combustion turbine at 100 percent load for t			_	_	
	in the duct burner for 8,760 hours per year a	nd operation at	the	site a	verage ambient	
	temperature of 73°F.	. 1651111 0	260	. 1 ,	× 1 . /0 000 11	
	Annual emissions = $(76.0 \text{ lb/hr} \times 500 \text{ hr/yr} - 27.1 \text{ tanglessor})$	+ 16.5 lb/hr x 8	,260	hr/yr	$(x + 1) \times (1 +$	
	87.1 tons/year					
9.	Pollutant Potential/Estimated Fugitive Emis	sions Commen	ıt:			
	Potential emissions shown in Fields 3 and 8				ng NO _x emission rates:	
	Combined cycle natural gas firing: 2.0 ppmvd at 15 percent O ₂					
	Combined cycle fuel oil firing: 8.0 ppmvd				1.1	
	Potential emission estimates are given for in limits.	itormational pu	irpos	ses and	d do not represent	
	minus.					

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### F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION -**ALLOWABLE EMISSIONS**

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

#### Allowable Emissions 1 of 4

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 0.0075 x (14.4/Y) + F in percent by volume at 15% oxygen and on a dry basis	4.	Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance: CEMS		
em	6. Allowable Emissions Comment (Description of Operating Method): The allowable emissions are from 40 CFR 60, Subpart GG and Rule 62-204.800(8)(b).39 - 40 CFR 60, Subpart GG Stationary Gas Turbines, adopted by reference.		

#### Allowable Emissions Allowable Emissions 2 of 4

1.	Basis for Allowable Emissions Code: OTHER	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 2.0 ppmvd at 15% O ₂ (combined cycle mode with natural gas firing)	4.	Equivalent Allowable Emissions: 17.5 lb/hour 72.3 tons/year
5	Method of Compliance: CEMS		

6. Allowable Emissions Comment (Description of Operating Method): The allowable emissions rate given in Field 3 is based on the BACT analysis provided with this application. Equivalent allowable emission rates are given for informational purposes only and do not represent limits. The equivalent allowable hourly emissions rate is based on operation at 100% load and an ambient temperature of 26°F. The equivalent annual allowable emissions rate is based on operation at 100% load for 8,760 hours per year and a site average ambient temperature of 73°F. The equivalent allowable emissions include emissions from HRSG duct burner firing. The allowable emissions from proposed 40 CFR 60, Subpart KKKK are 0.39 lb/MW-hr when firing natural gas, based on a 4-hour rolling average. If this proposed standard becomes final, compliance with the BACT levels will ensure compliance with the proposed standard.

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## POLLUTANT DETAIL INFORMATION Page [5] of [17]

## F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions 3 of 4

1. Basis f	For Allowable Emissions Code:	2.	Future Effective Date Emissions:	of Allowable
8.0 pp	able Emissions and Units: mvd at 15% O ₂ (combined cycle with fuel oil firing)	4.	Equivalent Allowable 81.1 lb/hour	Emissions: 20.3 tons/year
5. Metho	d of Compliance: CEMS			

6 Allowable Emissions Comment

6. Allowable Emissions Comment (Description of Operating Method): The allowable emissions rate given in Field 3 is based on the BACT analysis provided with this application. Equivalent allowable emission rates are given for informational purposes only and do not represent limits. The equivalent allowable hourly emissions rate is based on operation at 100% load and an ambient temperature of 26°F. The equivalent annual allowable emissions rate is based on operation at 100% load for 500 hours per year and a site minimum ambient temperature of 26°F. The equivalent allowable emissions include emissions from HRSG duct burner firing. The allowable emissions from proposed 40 CFR 60, Subpart KKKK are 1.2 lb/MW-hr when firing fuel oil, based on a 4-hour rolling average. If this proposed standard becomes final, compliance with the BACT levels will ensure compliance with the proposed standard.

#### Allowable Emissions Allowable Emissions 4 of 4

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions:
	0.20 lb/mmBtu (30-day rolling average)		113.1 lb/hour 495.2 tons/year
5	Method of Compliance: CEMS		

6. Allowable Emissions Comment (Description of Operating Method): The allowable emissions are from 40 CFR 60, Subpart Da and Rule 62-204.800(8)(b).3 - 40 CFR 60, Subpart Da, adopted by reference. The allowable emissions standard apply to the duct burner and are given at 40 CFR 60.44a(a)(1). The equivalent allowable emissions are based on a duct burner heat input rate of 565.3 mmBtu/hr (HHV). This emissions standard applies at all times except during periods of startup, shutdown or malfunction.

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## POLLUTANT DETAIL INFORMATION Page [5] of [17]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions	of
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:
	lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description	n of Operating Method):
Allowable Emissions Allowable Emissions	of
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description	n of Operating Method):

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## POLLUTANT DETAIL INFORMATION Page [7] of [17]

# F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted: PM	2. Total Perce	ent Efficie	ency of Control:
3.	Potential Emissions:		4. Synth	etically Limited?
	52.0 lb/hour 169.4	tons/year	х	Yes No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
	to tons/year			
6.	Emission Factor:			7. Emissions
		ć.		Method Code:
	Reference: Vendor Data			5
8.	Calculation of Emissions:			
	Potential emissions are based on vendor data.			
	The maximum hourly potential PM emissions are based on firing fuel oil in the combustion			
	turbine at 100% load, firing natural gas in the duct burner and operation at an ambient			
	temperature of 26°F. The maximum hourly			
	The maximum annual potential PM emissio		_	
	combustion turbine at 100 percent load for 5			
	combustion turbine at 100 percent load for t		•	
	in the duct burner for 8,760 hours per year a	nd operation at	the site av	verage ambient
	temperature of 73°F.		2601 ( )	
	Annual emissions = $(49.9 \text{ lb/hr x } 500 \text{ hr/yr})$	$+ 38.0 \text{ lb/hr } \times 8$	,260 hr/yr)	$) \times 1 \text{ ton/2,000 lb} =$
	169.4 tons/year			
9.	Pollutant Potential/Estimated Fugitive Emis			
	Potential emissions shown in Fields 3 and 8			
	Potential emission estimates are given for in	nformational pu	rposes and	d do not represent
	limits.			

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## POLLUTANT DETAIL INFORMATION Page [8] of [17]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions	_ of		
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5. Method of Compliance:			
6. Allowable Emissions Comment (Description	on of Operating Method):		
Allowable Emissions Allowable Emissions	_ of		
Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5. Method of Compliance:			
6. Allowable Emissions Comment (Description	on of Operating Method):		
Allowable Emissions Allowable Emissions	_ of		
Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5. Method of Compliance:			
6. Allowable Emissions Comment (Description of Operating Method):			

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# F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     PM10	2. Total Percent Efficiency of Control:				
3. Potential Emissions: 52.0 lb/hour 169.4	4. Synthetically Limited?  4 tons/year				
5. Range of Estimated Fugitive Emissions (as to tons/year					
6. Emission Factor:  Reference: Vendor Data	7. Emissions Method Code: 5				
ambient temperature of 26°F. The maximum The maximum annual potential PM ₁₀ emiss combustion turbine at 100 percent load for sombustion turbine at 100 percent load for the duct burner for 8,760 hours per year attemperature of 73°F.  Annual emissions = (49.9 lb/hr x 500 hr/yr 169.4 tons/year	ions are based on firing fuel oil in the ural gas in the duct burner and operation at an m hourly PM ₁₀ emission rate is 52.0 lb/hour. ions are based on firing fuel oil in the 500 hours per year, firing natural gas in the the remainder of the year, and firing natural gas and operation at the site average ambient + 38.0 lb/hr x 8,260 hr/yr) x 1 ton/2,000 lb =				
<ol> <li>Pollutant Potential/Estimated Fugitive Emis Potential emissions shown in Fields 3 and 8 Potential emission estimates are given for in limits.</li> </ol>	are based on front and back half catch.				

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## POLLUTANT DETAIL INFORMATION Page [10] of [17]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

<u>Al</u>	lowable Emissions Allowable Emissions	of
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions:
		lb/hour tons/year
5.	Method of Compliance:	
6.	Allowable Emissions Comment (Description	n of Operating Method):
Al	lowable Emissions Allowable Emissions	of
1.	Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
	Method of Compliance:  Allowable Emissions Comment (Description	n of Operating Method):
 Al	lowable Emissions Allowable Emissions	
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:	
6.	Allowable Emissions Comment (Description	n of Operating Method):

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## POLLUTANT DETAIL INFORMATION Page [11] of [17]

# F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted:	2. Total Perce	ent Efficie	ency of Control:
	SO2			
3.	Potential Emissions:		4. Synth	etically Limited?
	13.6 lb/hour 56.5	5 tons/year	х	Yes No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
	to tons/year			
6.	Emission Factor:			7. Emissions
				Method Code:
]	Reference: Vendor Data			5
8.	Calculation of Emissions:			
	Potential emissions are based on vendor dat	-	-	
	grains per 100 scf and ULS fuel oil with a 0	.0015 percent st	ulfur conte	ent.
	The maximum hourly potential SO ₂ emission	ons are based on	firing nat	ural gas in the
	combustion turbine at 100% load, firing natural gas in the duct burner and operation at an			
	ambient temperature of 26°F. The maximum	m hourly SO ₂ er	nission ra	te is 13.6 lb/hour.
	The maximum annual potential SO ₂ emission	ons are based on	firing nat	tural gas in the
	combustion turbine at 100% load, firing nat			
	site average ambient temperature of 73°F fo	•		•
	Annual emissions = $12.9 \text{ lb/hr} \times 8,760 \text{ hours/year} \times 1 \text{ ton/}2,000 \text{ lb} = 56.5 \text{ tons/year}$			56.5 tons/year
		•		·
	·			
9.	Pollutant Potential/Estimated Fugitive Emis			
	Potential emissions shown in Fields 3 and 8	are based on us	sing natura	al gas with a sulfur
	content of 2 grains per 100 scf. Use of ULS	fuel oil (0.001:	5 percent s	sulfur) results in lower
	SO ₂ emissions than with natural gas use. The			
	estimated effects of SO ₂ oxidation. Potential emission estimates are given for			given for
	informational purposes and do not represent			-

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## F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

#### Allowable Emissions 1 of 3

1.	Basis for Allowable Emissions Code: RULE	2.	Future Effective Da Emissions:	ate of Allowable
3.	Allowable Emissions and Units: 0.8% sulfur by weight in the fuel	4.	Equivalent Allowal lb/hour	ble Emissions: tons/year
5.	. Method of Compliance: Fuel testing and monitoring will be conducted in accordance with 40 CFR 60 Subpart GG, AS REVISED JULY 8, 2004.			

6. Allowable Emissions Comment (Description of Operating Method): The allowable emissions are from 40 CFR 60, Subpart GG and Rule 62-204.800(8)(b).39 - 40 CFR 60, Subpart GG Stationary Gas Turbines, adopted by reference.

#### Allowable Emissions 2 of 3

Basis for Allowable Emissions Code:     OTHER	2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units: 0.0015% sulfur by weight in the fuel oil	4. Equivalent Allowable Emissions: 6.3 lb/hour 1.6 tons/year

5. Method of Compliance: Fuel testing.

6. Allowable Emissions Comment (Description of Operating Method): The allowable emissions standard given in Field 3 is based on the BACT analysis provided with this application. Equivalent allowable emission rates are given for informational purposes only and do not represent limits. The equivalent allowable hourly emissions rate is based on operation at 100% load and an ambient temperature of 26°F. The equivalent annual allowable emissions rate is based on operation at 100% load for 500 hours per year and a site minimum ambient temperature of 26°F. The equivalent allowable emissions include the effects of firing natural gas in the HRSG duct burner. Excluding the effects of firing natural gas in the HRSG duct burner would result in equivalent allowable emission rates of 3.1 lb/hr and 0.8 tons/year. Meeting this proposed fuel sulfur emissions standard will also ensure compliance with the fuel sulfur standards included in NSPS Subpart GG and in proposed NSPS Subpart KKKK.

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## POLLUTANT DETAIL INFORMATION Page [13] of [17]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions 3 of 3

1.	Basis for Allowable Emissions Code: OTHER	2.	Future Effective Date Emissions:	of Allowable
3.		4.	Equivalent Allowable	
	2 grains sulfur per 100 scf in the natural gas		13.6 lb/hour	56.5 tons/year
5.	Method of Compliance: Compliance will be from the vendor indicating the average sulfur pipeline for each month of operation.		•	•
6.	Allowable Emissions Comment (Description emissions standard given in Field 3 is based application. Equivalent allowable emissions and do not represent limits. The equivalent a operation at 100% load in combined cycle mequivalent annual allowable emissions rate is cycle mode for 8,760 hours per year and a sit equivalent allowable emissions include the eburner. While the natural gas tariff does not sef, historical data indicates that this is a reast to include a natural gas sulfur content standards based on a calendar month average.	on the rates allow ode s bas te av ffect guars sona	ne BACT analysis provare given for informativable hourly emissions and an ambient tempered on operation at 100 erage ambient temperates of firing natural gas is rantee a sulfur content ble sulfur level. There	rided with this ional purposes only rate is based on rature of 26°F. The % load in combined ture of 73°F. The in the HRSG duct of 2 grains per 100 fore, if the permit is

### Allowable Emissions _ of _

1.	Basis for Allowable Emissions Code:	2.	Future Effective Date Emissions:	of Allowable
3.	Allowable Emissions and Units:	4.	Equivalent Allowable lb/hour	Emissions: tons/year
5.	Method of Compliance:			
6.	Allowable Emissions Comment (Description	of (	Operating Method):	

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## POLLUTANT DETAIL INFORMATION Page [14] of [17]

# F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     VOC	2. Total Percent Efficie	ency of Control:			
3. Potential Emissions:		netically Limited?			
10.2 lb/hour 23.	l tons/year x	Yes No			
5. Range of Estimated Fugitive Emissions (as	applicable):				
to tons/year					
6. Emission Factor:		7. Emissions			
		Method Code:			
Reference: Vendor Data		5			
8. Calculation of Emissions:					
Potential emissions are based on vendor dat					
The maximum hourly potential emissions as	_	_			
oil in the combustion turbine, firing natural					
temperature of 26°F. The maximum hourly VOC emission rate is 10.2 lb/hour.					
The maximum annual potential VOC emissions are based on firing fuel oil in the					
combustion turbine at 100 percent load for 500 hours per year, firing natural gas in the combustion turbine at 100 percent load for the remainder of the year, and firing natural gas					
in the duct burner for 8,760 hours per year and operation at the site average ambient					
temperature of 73°F.					
Annual emissions = $(9.7 \text{ lb/hr} \times 500 \text{ hr/yr} + 5.0 \text{ lb/hr} \times 8,260 \text{ hr/yr}) \times 1 \text{ ton/2,000 lbs} =$					
23.1 tons/year	0,000 10,111 11 0,200 111,717 11	2 4012 2,000 100			
9. Pollutant Potential/Estimated Fugitive Emis	sions Comment: Potenti	al emission estimates			
are given for informational purposes and do not		ar christian estimates			
	1				

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#### POLLUTANT DETAIL INFORMATION Page [15] of [17]

### F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION -**ALLOWABLE EMISSIONS**

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emi	ssions of
1. Basis for Allowable Emissions Co.	de:  2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:
	lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (D	Description of Operating Method):
Allowable Emissions Allowable Emi	ssions of
Basis for Allowable Emissions Co	de:  2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (D	Description of Operating Method):
Allowable Emissions Allowable Emi	ssions of
Basis for Allowable Emissions Co.	de:  2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (D	Description of Operating Method):

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POLLUTANT DETAIL INFORMATION
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## F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted:	2. Total Perc	ent Efficie	ency of Control:		
	SAM		_			
3.	Potential Emissions:		4. Synth	netically Limited?		
	5.5 lb/hour 22.4	tons/year	х	Yes 🔲 No		
5.	Range of Estimated Fugitive Emissions (as	applicable):				
	to tons/year					
6.	Emission Factor:			7. Emissions		
			'	Method Code:		
]	Reference: Vendor Data			5		
8.	Calculation of Emissions:					
	Potential emissions are based on vendor data	-	_			
	grains per 100 scf and ULS fuel oil with a 0	-				
	The maximum hourly potential sulfuric acid			0 0		
	in the combustion turbine at 100% load, firing natural gas in the duct burner and operation					
	at an ambient temperature of 26°F. The maximum hourly sulfuric acid mist emission rate					
	is 5.5 lb/hour.					
	The maximum annual potential sulfuric acid mist emissions are based on firing natural gas					
	in the combustion turbine at 100% load, firing natural gas in the duct burner and operation					
	at the site average ambient temperature of 73°F for 8,760 hours per year.					
	Annual emissions = $5.12 \text{ lb/hr} \times 8,760 \text{ hour}$	s/year x 1 ton/2	000 lb = 2	22.4 tons/year		
9.	Pollutant Potential/Estimated Fugitive Emis					
	Potential emissions shown in Fields 3 and 8		-	•		
	content of 2 grains per scf. Use of ULS fue					
	sulfuric acid mist emissions than with natur			ssion estimates are		
	given for informational purposes and do not	represent limit	S.			

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## F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

#### Allowable Emissions 1 of 2

Basis for Allowable Emissions Code:     OTHER	Future Effective Date of Allowable     Emissions:
<ol> <li>Allowable Emissions and Units:</li> <li>0.0015% sulfur by weight in the fuel oil</li> </ol>	4. Equivalent Allowable Emissions: 2.1 lb/hour 0.5 tons/year

5. Method of Compliance: Fuel testing

6. Allowable Emissions Comment (Description of Operating Method): The allowable emissions rate given in Field 3 is based on the BACT analysis provided with this application. Equivalent allowable emission rates are based on the estimated oxidation of SO₂ to SO₃ and assuming 100 percent conversion of SO₃ to sulfuric acid mist. Equivalent allowable emissions are given for informational purposes only and do not represent limits. The equivalent allowable hourly emissions rate is based on operation at 100% load and an ambient temperature of 26°F. The equivalent annual allowable emissions rate is based on operation at 100% load for 500 hours per year and a site minimum ambient temperature of 26°F. The equivalent allowable emissions include the effects of firing natural gas in the HRSG duct burner.

#### Allowable Emissions Allowable Emissions 2 of 2

Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units: 2 grains sulfur per 100 scf in the natural gas	4. Equivalent Allowable Emissions: 5.5 lb/hour 22.4 tons/year
5 N 4 1 CO - 1 E 141	<u> </u>

5. Method of Compliance: Fuel testing

6. Allowable Emissions Comment (Description of Operating Method): The allowable emissions rate given in Field 3 is based on the BACT analysis provided with this application. Equivalent allowable emission rates are based on the estimated oxidation of SO₂ to SO₃ and assuming 100 percent conversion of SO₃ to sulfuric acid mist. Equivalent allowable emissions are given for informational purposes only and do not represent limits. The equivalent allowable hourly emissions rate is based on operation at 100% load and an ambient temperature of 26°F. The equivalent annual allowable emissions rate is based on operation at 100% load for 8,760 hours per year and a site average ambient temperature of 73°F. The equivalent allowable emissions include the effects of firing natural gas in the HRSG duct burner.

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### **EMISSIONS UNIT INFORMATION**

Section [1]

of [6]

#### G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

<u>Visible Emissions Limitation:</u> Visible Emissions Limitation of						
1.	Visible Emissions Subtype:		2. Basis for Allowable	Opacity:		
	-		☐ Rule	Other		
3.	Allowable Opacity:		•			
	Normal Conditions:	% E:	xceptional Conditions:	%		
	Maximum Period of Excess Opac	ity Allow	red:	min/hour		
4.	Method of Compliance:					
5.	Visible Emissions Comment:					
¥.7°		1 5				
<u>Vi</u>	sible Emissions Limitation: Visib	ole Emiss	ions Limitation of			
	sible Emissions Limitation: Visib	ole Emiss	2. Basis for Allowable	2		
		ole Emiss		Opacity:		
1.	Visible Emissions Subtype:  Allowable Opacity:		2. Basis for Allowable   Rule	Other		
1.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions:	% E	2. Basis for Allowable Rule	Other %		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac	% E	2. Basis for Allowable Rule	Other		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions:	% E	2. Basis for Allowable Rule	Other %		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac	% E	2. Basis for Allowable Rule	Other %		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac	% E	2. Basis for Allowable Rule	Other %		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac Method of Compliance:	% E	2. Basis for Allowable Rule	Other %		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac Method of Compliance:	% E	2. Basis for Allowable Rule	Other %		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac Method of Compliance:	% E	2. Basis for Allowable Rule	Other %		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac Method of Compliance:	% E	2. Basis for Allowable Rule	Other %		

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### H. CONTINUOUS MONITOR INFORMATION

### Complete if this emissions unit is or would be subject to continuous monitoring.

Continuous Monitoring System: Continuous Monitor 1 of 2

1. Parameter Code: EM	2. Pollutant(s): NOX
3. CMS Requirement:	x Rule Other
Monitor Information     Manufacturer: To be determined     Model Number: To be determined	Serial Number: To be determined
5. Installation Date:	6. Performance Specification Test Date:
7. Continuous Monitor Comment: CEMS will source. CEMS is required as a condition of 40	<del>-</del>
Continuous Monitoring System: Continuous	Monitor 2 of 2
1. Parameter Code: CO2 or O2	2. Pollutant(s):
3. CMS Requirement:	x Rule Other
4. Monitor Information  Manufacturer: To be determined	
Model Number: To be determined	Serial Number: To be determined
5. Installation Date:	6. Performance Specification Test Date:
7. Continuous Monitor Comment: CEMS will source. CEMS is required as a condition of 40	- '

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### H. CONTINUOUS MONITOR INFORMATION (CONTINUED)

Complete if this emissions unit is or would be subject to continuous monitoring.

<u>Continuous Monitoring System:</u> Continuous Monitor _ of _

1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	Rule Other
4.	Monitor Information  Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
Co	ntinuous Monitoring System: Continuous	Monitor _ of _
1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	Rule Other
4.	Monitor Information Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	

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### EMISSIONS UNIT INFORMATION

Section [1] of [6]

#### I. EMISSIONS UNIT ADDITIONAL INFORMATION

### Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)            x         Attached, Document ID: Attach. B         Previously Submitted, Date
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)     Attached, Document ID: Attach. L Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  X Attached, Document ID: Attach. M Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)    X   Attached, Document ID: Attach. N   Previously Submitted, Date
5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)   X Attached, Document ID: Attach. O Previously Submitted, Date  Not Applicable
6.	Compliance Demonstration Reports/Records  Attached, Document ID:  Test Date(s)/Pollutant(s) Tested:
	Previously Submitted, Date:  Test Date(s)/Pollutant(s) Tested:
	To be Submitted, Date (if known):  Test Date(s)/Pollutant(s) Tested:
	x Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute  Attached, Document ID: x Not Applicable

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### **EMISSIONS UNIT INFORMATION**

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### **Additional Requirements for Air Construction Permit Applications**

1. Control Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7), F.A.C.; 40 CFR 63.43(d) and (e))	
X Attached, Document ID: Attach. P Not Applicable	
2. Good Engineering Practice Stack Height Analysis (Rule 62-212.400(5)(h)6., F.A.C., and Rule 62-212.500(4)(f), F.A.C.)	
x Attached, Document ID: Attach. Q Not Applicable	
3. Description of Stack Sampling Facilities (Required for proposed new stack sampling facilities only)	
x Attached, Document ID: Attach. R Not Applicable	
Additional Requirements for Title V Air Operation Permit Applications	
Identification of Applicable Requirements     Attached, Document ID:	
2. Compliance Assurance Monitoring  Attached, Document ID: Not Applicable	
3. Alternative Methods of Operation  Attached, Document ID: Not Applicable	
4. Alternative Modes of Operation (Emissions Trading)	
□ Certificate of Representation (EPA Form No. 7610-1)   □ Copy Attached, Document ID:   □ Acid Rain Part (Form No. 62-210.900(1)(a))   □ Attached, Document ID:   □ Previously Submitted, Date:   □ Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)   □ Attached, Document ID:   □ Previously Submitted, Date:   □ New Unit Exemption (Form No. 62-210.900(1)(a)2.)   □ Attached, Document ID:   □ Previously Submitted, Date:   □ Previously Submitted, Date:   □ Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)   □ Attached, Document ID:   □ Previously Submitted, Date:   □ Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)   □ Attached, Document ID:   □ Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)   □ Attached, Document ID:   □ Attached, Document ID:	
☐ Previously Submitted, Date:	

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Additional Requirements Comment				

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#### III. EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Application - For Title V air operation permitting only, emissions units are classified as regulated, unregulated, or insignificant. If this is an application for Title V air operation permit, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each regulated and unregulated emissions unit addressed in this application for air permit. Some of the subsections comprising the Emissions Unit Information Section of the form are optional for unregulated emissions units. Each such subsection is appropriately marked. Insignificant emissions units are required to be listed at Section II, Subsection C.

Air Construction Permit or FESOP Application - For air construction permitting or federally enforceable state air operation permitting, emissions units are classified as either subject to air permitting or exempt from air permitting. The concept of an "unregulated emissions unit" does not apply. If this is an application for air construction permit or FESOP, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air permitting are required to be listed at Section II, Subsection C.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit Application — Where this application is used to apply for both an air construction permit and a revised/renewal Title V air operation permit, each emissions unit is classified as either subject to air permitting or exempt from air permitting for air construction permitting purposes and as regulated, unregulated, or insignificant for Title V air operation permitting purposes. The air construction permitting classification must be used to complete the Emissions Unit Information Section of this application for air permit. A separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air construction permitting and insignificant emissions units are required to be listed at Section II, Subsection C.

If submitting the application form in hard copy, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application must be indicated in the space provided at the top of each page.

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#### A. GENERAL EMISSIONS UNIT INFORMATION

### Title V Air Operation Permit Emissions Unit Classification

	1. Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)							
	<ul> <li>The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.</li> <li>The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.</li> </ul>							
_	Emissions Unit Description and Status							
ſ	1. Type of Emissions Unit Addresse	ed in this Sectio	n: (Check one)					
This Emissions Unit Information Section addresses, as a single emissions unit, a								
	single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).							
	This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.							
	This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only.							
2. Description of Emissions Unit Addressed in this Section: Auxiliary Boiler.								
	3. Emissions Unit Identification Nu	ımber:						
	4. Emissions Unit Status Code: C	6. Initial Startup Date:	7. Emissions Unit Major Group SIC Code: 49	8. Acid Rain Unit?  Yes  No				
	Package Unit:     Manufacturer: TBD		Model Number: TBI	)				
	10. Generator Nameplate Rating:							
	11. Emissions Unit Comment:							

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### **Emissions Unit Control Equipment**

1. Control Equipment/Method(s) Description:						
2. Control Device or Method Code(s):						

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### **B. EMISSIONS UNIT CAPACITY INFORMATION**

(Optional for unregulated emissions units.)

### **Emissions Unit Operating Capacity and Schedule**

1.	Maximum Process or Throughput Rate:				
2.	Maximum Production Rate:				
3.	. Maximum Heat Input Rate: 7.2 mmBtu/hr (estimate)				
4.	Maximum Incineration Rate: pounds/hr				
	tons/day				
5.	5. Requested Maximum Operating Schedule:				
	24 hours/day	7 days/week			
	52 weeks/year	8,760 hours/year			
6.	Operating Capacity/Schedule Comment: The maximum heat input rat an estimate. The actual maximum heat input rate will be dependent or	•			

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# C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

### **Emission Point Description and Type**

1.	Identification of Point on l	Plot Plan or	2.	<b>Emission Point T</b>	ype Code:
	Flow Diagram: Auxiliary	Boiler		1	
	Descriptions of Emission				J
5.	5. Discharge Type Code: 6. Stack Height: 7. Exit Diameter: 1.3 feet				
8.	Exit Temperature: 525°F	9. Actual Volum 2,600 acfm	netr	ic Flow Rate:	10. Water Vapor:
11	. Maximum Dry Standard F dscfm	Flow Rate:	12.	Nonstack Emissi	on Point Height:
13	13. Emission Point UTM Coordinates  Zone: 17 East (km): 561.5523  North (km): 3028.9614		14. Emission Point Latitude/Longitude Latitude (DD/MM/SS) Longitude (DD/MM/SS)		
15	15. Emission Point Comment: The above information is based on preliminary vendor information and represents the expected emission unit parameters. A specific auxiliary boiler model has not been chosen yet.				

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### EMISSIONS UNIT INFORMATION

Section [2] of [6]

### D. SEGMENT (PROCESS/FUEL) INFORMATION

### Segment Description and Rate: Segment 1 of 1

1.	. Segment Description (Process/Fuel Type): Natural gas used in the auxiliary boiler					
2.	2. Source Classification Code (SCC): 10100602		3. SCC Units: Million Cubic Feet Burned			
4.	Maximum Hourly Rate: 0.0074	5. Maximum . 64.8	Annual Rate:	6.	Estimated Annual Activity Factor:	
7.	Maximum % Sulfur:	8. Maximum	% Ash:	9.	Million Btu per SCC Unit: 970 (HHV)	
Se	gment Description and Ra		of			
1.	1. Segment Description (Process/Fuel Type):					
2.	2. Source Classification Code (SCC):  3. SCC Units:					
4.	Maximum Hourly Rate:	5. Maximum	Annual Rate:	6.	Estimated Annual Activity Factor:	
7.	Maximum % Sulfur:	8. Maximum % Ash:		9.	Million Btu per SCC Unit:	
10	. Segment Comment:					

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### E. EMISSIONS UNIT POLLUTANTS

### List of Pollutants Emitted by Emissions Unit

1. Pollutant Emitted	Primary Control     Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
СО			NS
NOX			NS
PM			NS
PM10			NS
SO2			NS
VOC			NS
			<u> </u>
<u> </u>			
-			

### POLLUTANT DETAIL INFORMATION [1] of [12]

## F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     CO	2. Total Percent Efficiency of Control:
3. Potential Emissions:	4. Synthetically Limited?
0.52 lb/hour 2.2	8 tons/year Yes x No
5. Range of Estimated Fugitive Emissions (as	applicable):
to tons/year	
6. Emission Factor:	7. Emissions
	Method Code:
Reference: Vendor Data	5
8. Calculation of Emissions:	
Potential emissions are based on vendor dat	
The maximum hourly CO emission rate is 0	
The maximum annual potential CO emissio	ns are based on operation for 8,760 hours per
year.	
Annual emissions = $0.52$ lb/hr x 8,760 hour	s/year x 1 ton/2,000 lb = $2.28$ tons/year
	·
9. Pollutant Potential/Estimated Fugitive Emis	ssions Comment:
The potential emissions are estimates based	
emissions are given for informational purpo	ses and do not represent limits.

## POLLUTANT DETAIL INFORMATION Page [2] of [12]

## F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions	_ of				
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:				
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:				
	lb/hour tons/year				
5. Method of Compliance:					
6. Allowable Emissions Comment (Description of Operating Method):					
Allowable Emissions	_ of				
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:				
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year				
5. Method of Compliance:	·				
6. Allowable Emissions Comment (Description of Operating Method):					
Allowable Emissions	_ of				
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:				
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year				
5. Method of Compliance:					
6. Allowable Emissions Comment (Description	n of Operating Method):				

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### POLLUTANT DETAIL INFORMATION Page [3] of [12]

## F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     NOX	2. Total Percent Efficie	ency of Control:
3. Potential Emissions:	4. Synth	netically Limited?
0.26 lb/hour 1.14	4 tons/year Y	es x No
5. Range of Estimated Fugitive Emissions (as	applicable):	
to tons/year		
6. Emission Factor:		7. Emissions
Reference: Vendor Data		Method Code: 5
8. Calculation of Emissions:  Potential emissions are based on vendor data.  The maximum hourly NO _x emission rate is 0.26 lb/hour.  The maximum annual potential NO _x emissions are based on operation for 8,760 hours per year.  Annual emissions = 0.26 lb/hr x 8,760 hours/year x 1 ton/2,000 lb = 1.14 tons/year		
Pollutant Potential/Estimated Fugitive Emissions Comment: The potential emissions are estimates based on preliminary vendor data. The potential emissions are given for informational purposes and do not represent limits.		

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## POLLUTANT DETAIL INFORMATION Page [4] of [12]

## F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions _ of _				
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:			
	lb/hour tons/year			
5. Method of Compliance:				
6. Allowable Emissions Comment (Description of Operating Method):				

#### Allowable Emissions Allowable Emissions of

1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:	
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions:	
			lb/hour tons/year	
5.	Method of Compliance:			
6.	Allowable Emissions Comment (Description	of (	Operating Method):	

POLLUTANT DETAIL INFORMATION
Page [5] of [12]

## F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     PM	2. Total Percent Efficiency of Control:					
3. Potential Emissions: 0.03 lb/hour 0.13	4. Synthetically Limited?  3 tons/year Yes x No					
5. Range of Estimated Fugitive Emissions (as to tons/year						
6. Emission Factor:  Reference: Vendor Data	7. Emissions Method Code: 5					
8. Calculation of Emissions: Potential emissions are based on vendor data. The maximum hourly PM emission rate is 0.03 lb/hour. The maximum annual potential PM emissions are based on operation for 8,760 hours per year. Annual emissions = 0.03 lb/hr x 8,760 hours/year x 1 ton/2,000 lb = 0.13 tons/year						
9. Pollutant Potential/Estimated Fugitive Emis The potential emissions are estimates based emissions are given for informational purpo	on preliminary vendor data. The potential					

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## POLLUTANT DETAIL INFORMATION Page [6] of [12]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions	_ of
1. Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description	on of Operating Method):
Allowable Emissions _	_ of
Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description	on of Operating Method):
<u>Allowable Emissions</u> Allowable Emissions	_ of
Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description	on of Operating Method):

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POLLUTANT DETAIL INFORMATION
Page [7] of [12]

# F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1. Pollutant Emitted: PM10	2. Total Percent Efficiency of Control:		
3. Potential Emissions:	4. Synthetically Limited?		
0.03 lb/hour 0.13	3 tons/year Yes x No		
5. Range of Estimated Fugitive Emissions (as	applicable):		
to tons/year			
6. Emission Factor:	7. Emissions		
	Method Code:		
Reference: Vendor Data	5		
8. Calculation of Emissions: Potential emissions are based on vendor data. The maximum hourly PM ₁₀ emission rate is 0.03 lb/hour. The maximum annual potential PM ₁₀ emissions are based on firing operation for 8,760 hours per year. Annual emissions = 0.03 lb/hr x 8,760 hours/year x 1 ton/2,000 lb = 0.13 tons/year			
<ol> <li>Pollutant Potential/Estimated Fugitive Emissions Comment:         The potential emissions are estimates based on preliminary vendor data. The potential emissions are given for informational purposes and do not represent limits.     </li> </ol>			

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## POLLUTANT DETAIL INFORMATION Page [8] of [12]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

<u>Allo</u>	wable Emissions Allowable Emissions	_ of
1.	Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions:
		lb/hour tons/year
5.	Method of Compliance:	
6.	Allowable Emissions Comment (Description	n of Operating Method):
Alla	owable Emissions Allowable Emissions	of
	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable
1.	Dasis for Anowabic Emissions Code.	Emissions:
3	Allowable Emissions and Units:	4. Equivalent Allowable Emissions:
		lb/hour tons/year
5.	Method of Compliance:	
6.	Allowable Emissions Comment (Description	n of Operating Method):
Allo	owable Emissions Allowable Emissions	_ of
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
2	Allowable Emissions and Units:	
3. 1	Allowable Emissions and Units:	4. Equivalent Allowable Emissions:    lb/hour   tons/year
5 1	Method of Compliance:	10/110di tolis/year
3. 1	wiemod of Comphance.	
6.	Allowable Emissions Comment (Description	n of Operating Method):
	( <b>200</b>	or of treaton).

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### POLLUTANT DETAIL INFORMATION Page [9] of [12]

## F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     SO2	2. Total Percent Efficiency of Control:	
3. Potential Emissions: 0.04 lb/hour 0.1	4. Synthetically Limited?  8 tons/year Yes x No	
5. Range of Estimated Fugitive Emissions (as to tons/year	applicable):	
6. Emission Factor:  Reference: Vendor Data	7. Emissions Method Code: 5	
2 grains per 100 scf.  The maximum hourly SO ₂ emission rate is The maximum annual potential SO ₂ emission year.  Annual emissions = 0.04 lb/hr x 8,760 hour	ons are based on operation for 8,760 hours per rs/year x 1 ton/2,000 lb = 0.18 tons/year	
	B are based on using natural gas with a sulfur ial emissions are estimates based on preliminary	

## POLLUTANT DETAIL INFORMATION Page [10] of [12]

## F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

<u>Al</u>	lowable Emissions Allowable Emissions _ o	of	·
1.	Basis for Allowable Emissions Code:		Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:		
6.	Allowable Emissions Comment (Description	of O	Operating Method):
Al	lowable Emissions Allowable Emissions _ c	of_	
1.	Basis for Allowable Emissions Code:	1	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:		
6.	Allowable Emissions Comment (Description	of C	Operating Method):

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### POLLUTANT DETAIL INFORMATION Page [11] of [12]

# F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     VOC	2. Total Percent Efficiency of Control:			
3. Potential Emissions:	4. Synthetically Limited?			
0.04 lb/hour 0.1	8 tons/year Yes x No			
5. Range of Estimated Fugitive Emissions (as to tons/year	s applicable):			
6. Emission Factor:	7. Emissions			
	Method Code:			
Reference: Vendor Data	5			
8. Calculation of Emissions:				
Potential emissions are based on vendor dat				
The maximum hourly VOC emission rate is				
_	sions are based on operation for 8,760 hours pe	r		
1 7	year.			
Annual emissions = $0.04 \text{ lb/hr} \times 8,760 \text{ hours/year} \times 1 \text{ ton/2,000 lbs} = 0.18 \text{ tons/year}$				
O. D. H. david Datamtic I/Estimated Fraction Facilities				
	ssions Comment: The potential emissions are			
	estimates based on preliminary vendor data. The potential emissions are given for			
informational purposes and do not represent	a mms.			

Allowable Emissions __ of ___

## POLLUTANT DETAIL INFORMATION Page [12] of [12]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

1. B	Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:		
3. A	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5. M	Method of Compliance:			
	Allowable Emissions Comment (Description		Operating Method):	
	wable Emissions Allowable Emissions Basis for Allowable Emissions Code:		Future Effective Date of Allowable Emissions:	
3. A	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year	
5. N	Method of Compliance:	•		
6. A	Allowable Emissions Comment (Description	of (	Operating Method):	
Allo	wable Emissions Allowable Emissions	of_	<u> </u>	
1. E	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:	
3. A	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year	
5. N	Method of Compliance:			
6. A	Allowable Emissions Comment (Description	n of	Operating Method):	

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#### G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

Visible Emissions Limitation: Visible Emissions Limitation of					
1.	Visible Emissions Subtype:	2. Basis for Allowal	ole Opacity:		
	VE20	x Rule	Other		
3.	Allowable Opacity:				
	Normal Conditions: 20 % Ex	ceptional Conditions:	27 %		
	Maximum Period of Excess Opacity Allow	ed:	6 min/hour		
4.	Method of Compliance: USEPA Method 9	visual determination o	f opacity		
5.	Visible Emissions Comment: Rule 62-296.	406 F A C			
5.	VISIOLE EMISSIONS COMMENT. Rule 02-270.	100, 1 .7 i.C.			
	- · · · · · · · · · · · · · · · · · · ·				
Vi	sible Emissions Limitation: Visible Emissi	ons Limitation of			
	sible Emissions Limitation: Visible Emissi Visible Emissions Subtype:	ons Limitation of _			
1.	Visible Emissions Subtype:  Allowable Opacity:	2. Basis for Allowal	ole Opacity:		
1.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Ex	2. Basis for Allowal Rule Ceptional Conditions:	ole Opacity:  Other		
1.	Visible Emissions Subtype:  Allowable Opacity:	2. Basis for Allowal Rule Ceptional Conditions:	ole Opacity:  Other		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Ex	2. Basis for Allowal Rule Ceptional Conditions:	ole Opacity:  Other		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Ex Maximum Period of Excess Opacity Allow	2. Basis for Allowal Rule Ceptional Conditions:	ole Opacity:  Other		
1.     3.     4.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Ex Maximum Period of Excess Opacity Allow Method of Compliance:	2. Basis for Allowal Rule Ceptional Conditions:	ole Opacity:  Other		
1.     3.     4.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Ex Maximum Period of Excess Opacity Allow	2. Basis for Allowal Rule Ceptional Conditions:	ole Opacity:  Other		
1.     3.     4.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Ex Maximum Period of Excess Opacity Allow Method of Compliance:	2. Basis for Allowal Rule Ceptional Conditions:	ole Opacity:  Other		
1.     3.     4.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Ex Maximum Period of Excess Opacity Allow Method of Compliance:	2. Basis for Allowal Rule Ceptional Conditions:	ole Opacity:  Other		
1.     3.     4.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Ex Maximum Period of Excess Opacity Allow Method of Compliance:	2. Basis for Allowal Rule Ceptional Conditions:	ole Opacity:  Other		
1.     3.     4.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Ex Maximum Period of Excess Opacity Allow Method of Compliance:	2. Basis for Allowal Rule Ceptional Conditions:	ole Opacity:  Other		

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### H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

 Continuous Monitoring System:
 Continuous Monitor of _

 1. Parameter Code:
 2. Pollutant(s):

1. Takameter Code.	2. Torradam(s).
3. CMS Requirement:	Rule Other
4. Monitor Information  Manufacturer:	
Model Number:	Serial Number:
5. Installation Date:	6. Performance Specification Test Date:
7. Continuous Monitor Comment:	
Continuous Monitoring System: Continuous	Monitor _ of _
1. Parameter Code:	2. Pollutant(s):
3. CMS Requirement:	Rule Other
4. Monitor Information  Manufacturer:	
Model Number:	Serial Number:
5. Installation Date:	6. Performance Specification Test Date:
7. Continuous Monitor Comment:	

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#### **EMISSIONS UNIT INFORMATION**

Section [2]

of [6]

#### I. EMISSIONS UNIT ADDITIONAL INFORMATION

### Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID: Previously Submitted, Date
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)    x Attached, Document ID: Attach. L Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID: Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID: Previously Submitted, Date  Not Applicable (construction application)
5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)   X Attached, Document ID: Attach. O Previously Submitted, Date  Not Applicable
6.	Compliance Demonstration Reports/Records  Attached, Document ID:  Test Date(s)/Pollutant(s) Tested:
	Previously Submitted, Date:  Test Date(s)/Pollutant(s) Tested:
	To be Submitted, Date (if known):  Test Date(s)/Pollutant(s) Tested:
	× Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute  Attached, Document ID: × Not Applicable

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### **EMISSIONS UNIT INFORMATION**

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### Additional Requirements for Air Construction Permit Applications

1	ontrol Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7), A.C.; 40 CFR 63.43(d) and (e))
1	Attached, Document ID: Attach. P Not Applicable
1	ood Engineering Practice Stack Height Analysis (Rule 62-212.400(5)(h)6., F.A.C., and
1	lle 62-212.500(4)(f), F.A.C.)  Attached, Document ID: Attach. Q Not Applicable
	escription of Stack Sampling Facilities (Required for proposed new stack sampling
	cilities only)
	Attached, Document ID: X Not Applicable
<u>Addit</u>	ional Requirements for Title V Air Operation Permit Applications
1. Id	entification of Applicable Requirements
	Attached, Document ID:
ı	npliance Assurance Monitoring
	Attached, Document ID: Not Applicable
	ernative Methods of Operation
	Attached, Document ID: Not Applicable
4. Al	ernative Modes of Operation (Emissions Trading)
	Attached, Document ID: Not Applicable
5. Ac	id Rain Part Application
	Certificate of Representation (EPA Form No. 7610-1)
	Copy Attached, Document ID:_   Acid Rain Part (Form No. 62-210.900(1)(a))
	Acta Rain Fart (Point No. 02-210.900(1)(a))  Attached, Document ID:
	Previously Submitted, Date:
_	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
_	Attached, Document ID:
	Previously Submitted, Date:
	New Unit Exemption (Form No. 62-210.900(1)(a)2.)
	Attached, Document ID:
_	Previously Submitted, Date:
	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)  Attached, Document ID:
	Attached, Document ID: Previously Submitted, Date:
	Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)
	Attached, Document ID:
	Previously Submitted, Date:
	Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)
	Attached, Document ID:
	Previously Submitted, Date:
	Not Applicable

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Additional Requirements Comment					
-					

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#### **EMISSIONS UNIT INFORMATION**

Section [3]

of [6]

#### III. EMISSIONS UNIT INFORMATION

**Title V Air Operation Permit Application** - For Title V air operation permitting only, emissions units are classified as regulated, unregulated, or insignificant. If this is an application for Title V air operation permit, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each regulated and unregulated emissions unit addressed in this application for air permit. Some of the subsections comprising the Emissions Unit Information Section of the form are optional for unregulated emissions units. Each such subsection is appropriately marked. Insignificant emissions units are required to be listed at Section II, Subsection C.

Air Construction Permit or FESOP Application - For air construction permitting or federally enforceable state air operation permitting, emissions units are classified as either subject to air permitting or exempt from air permitting. The concept of an "unregulated emissions unit" does not apply. If this is an application for air construction permit or FESOP, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air permitting are required to be listed at Section II, Subsection C.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit Application — Where this application is used to apply for both an air construction permit and a revised/renewal Title V air operation permit, each emissions unit is classified as either subject to air permitting or exempt from air permitting for air construction permitting purposes and as regulated, unregulated, or insignificant for Title V air operation permitting purposes. The air construction permitting classification must be used to complete the Emissions Unit Information Section of this application for air permit. A separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air construction permitting and insignificant emissions units are required to be listed at Section II, Subsection C.

If submitting the application form in hard copy, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application must be indicated in the space provided at the top of each page.

DEP Form No. 62-210.900(1) – Form

### A. GENERAL EMISSIONS UNIT INFORMATION

### Title V Air Operation Permit Emissions Unit Classification

	1.	Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)				
	☐ The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit. ☐ The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.					
	En	<u>issions Unit</u>	Description and Sta	itus		
Γ	1.	Type of Emis	ssions Unit Addresse	d in this Sectio	n: (Check one)	
		x This	Emissions Unit Infor	mation Section	addresses, as a single	emissions unit, a
			-		which produces one on point (stack or vent)	-
					• '	issions unit, a group of
		•	•			finable emission point
		•	vent) but may also pr	•		
					lresses, as a single em es which produce fugi	
ľ	2.	Description of	of Emissions Unit Ad	ldressed in this	Section: Diesel Engi	ne Fire Pump.
ļ						
L	3.	_	nit Identification Nur			· · · · · · · · · · · · · · · · · · ·
١	4.	Emissions	5. Commence	6. Initial	7. Emissions Unit	8. Acid Rain Unit?
١		Unit Status Code:	Construction Date:	Startup Date:	Major Group SIC Code:	☐ Yes
		C C	Date.	Date.	49	
r	9.	Package Unit	t:			<u> </u>
L		Manufacture	r: TBD		Model Number: TBI	)
	10. Generator Nameplate Rating:					
	11. Emissions Unit Comment: The diesel engine fire pump is considered emergency equipment and as such is considered exempt from permitting in accordance with Rule 62-210.300(3). While this emissions unit is exempt from permitting its' emissions are still included in the potential to emit for the Project and in the AQIA and this Emissions Unit Information Section is used to provide information on the Diesel Engine Fire Pump.					
1						

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### **Emissions Unit Control Equipment**

1. Control Equipment/Method(s) Description:	
`	
2. Control Device or Method Code(s):	

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### **B. EMISSIONS UNIT CAPACITY INFORMATION**

(Optional for unregulated emissions units.)

### **Emissions Unit Operating Capacity and Schedule**

1.	Maximum Process or Throughput Rate:	
2.	Maximum Production Rate: 300 HP (approximate)	
3.	Maximum Heat Input Rate:	
4.	Maximum Incineration Rate: pounds/hr	
	tons/day	
5.	Requested Maximum Operating Schedule:	
	24 hours/day	7 days/week
	52 weeks/year	8,760 hours/year
6.	Operating Capacity/Schedule Comment: Based on National Fire Prote (NFPA) guidelines it is conservatively estimated that the diesel engine operate approximately 200 hours per year. Because this is emergency maximum operating schedule is not requested. Because a specific mathas not been determined, the maximum production rate provided is an	e fire pump will fire equipment, a nufacturer and model

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# C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

### **Emission Point Description and Type**

Identification of Point on I     Flow Diagram: Fire Pump		2. Emission Point 7	ype Code:
3. Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking:  4. ID Numbers or Descriptions of Emission Units with this Emission Point in Common:			
5. Discharge Type Code:	6. Stack Height 29 feet	i:	7. Exit Diameter: 0.835 feet
8. Exit Temperature: 708°F	9. Actual Volum 2,150 acfm	metric Flow Rate:	10. Water Vapor: %
11. Maximum Dry Standard Flow Rate: dscfm		12. Nonstack Emission Point Height:	
13. Emission Point UTM Coordinates  Zone: 17 East (km): 561.4285  North (km): 3028.9605		14. Emission Point I Latitude (DD/M Longitude (DD/I	•
15. Emission Point Comment: The above information is based on preliminary vendor information and represents the expected approximate emission unit parameters.			

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### D. SEGMENT (PROCESS/FUEL) INFORMATION

### Segment Description and Rate: Segment $\underline{1}$ of $\underline{1}$

Segment Description (Process/Fuel Type):     Fuel oil used in the diesel engine fire pump			
2. Source Classification Code 20100301	e (SCC):	3. SCC Units: Thousand C	Gallons Burned
4. Maximum Hourly Rate: 0.0166	5. Maximum 2 3.32	Annual Rate:	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur: 0.0015	8. Maximum	% Ash:	9. Million Btu per SCC Unit: 137 (HHV)
10. Segment Comment: The a and represents the expected based on an estimated 200	d approximate er	nission unit para	• • • • • • • • • • • • • • • • • • •
Segment Description and Ra	te: Segment _	of _	
1. Segment Description (Process/Fuel Type):			
2. Source Classification Code	e (SCC):	3. SCC Units	:
4. Maximum Hourly Rate:	5. Maximum	Annual Rate:	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur:	8. Maximum	% Ash:	9. Million Btu per SCC Unit:
10. Segment Comment:			

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### E. EMISSIONS UNIT POLLUTANTS

### List of Pollutants Emitted by Emissions Unit

1. Pollutant Emitted	Primary Control     Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
СО			NS
NOX			NS
PM			NS
PM10			NS
SO2			NS
VOC			NS
			·
·			
	_		
_			

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## POLLUTANT DETAIL INFORMATION [1] of [12]

## F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1. Pollutant Emitted: CO	2. Total Percent Effici	ency of Control:
3. Potential Emissions:	4. Synt	hetically Limited?
1.2 lb/hour 0.12	2 tons/year	res x No
5. Range of Estimated Fugitive Emissions (as to tons/year	applicable):	
6. Emission Factor:	Method Code:	
Reference: Vendor Data		5
8. Calculation of Emissions: Potential emissions are based on vendor data. The maximum hourly CO emission rate is 1.2 lb/hour. The maximum annual potential CO emissions are based on operating 200 hours per year. Annual emissions = 1.2 lb/hr x 200 hours/year x 1 ton/2,000 lb = 0.12 tons/year		
9. Pollutant Potential/Estimated Fugitive Emissions Comment: The potential emissions are estimates based on preliminary vendor data. The potential emissions are given for informational purposes and do not represent limits.		

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## POLLUTANT DETAIL INFORMATION Page [2] of [12]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

<u>Al</u>	Iowable Emissions Allowable Emissions	. OI
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions:
		lb/hour tons/year
5.	Method of Compliance:	
6.	Allowable Emissions Comment (Description	n of Operating Method):
<u>Al</u>	lowable Emissions Allowable Emissions	of
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:	
6. Allowable Emissions Comment (Description of Operating Method):		
Al	lowable Emissions Allowable Emissions	_ of
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:	
6.	Allowable Emissions Comment (Description	n of Operating Method):

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## POLLUTANT DETAIL INFORMATION Page [3] of [12]

## F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     NOX	2. Total Percent Efficiency of Control:	
3. Potential Emissions:	4. Synthetically Limited?	
5.9 lb/hour 0.59	tons/year Yes x No	
5. Range of Estimated Fugitive Emissions (as to tons/year	applicable):	
6. Emission Factor:	7. Emissions Method Code:	
Reference: Vendor Data	5	
8. Calculation of Emissions: Potential emissions are based on vendor data. The maximum hourly NO _x emission rate is 5.9 lb/hour. The maximum annual potential NO _x emissions are based on operating 200 hours per year. Annual emissions = 5.9 lb/hr x 200 hours/year x 1 ton/2,000 lb = 0.59 tons/year		
9. Pollutant Potential/Estimated Fugitive Emissions Comment: The potential emissions are estimates based on preliminary vendor data. The potential emissions are given for informational purposes and do not represent limits.		

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Allowable Emissions _ of _

## POLLUTANT DETAIL INFORMATION Page [4] of [12]

## F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:	
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year	
5. Method of Compliance:		
6. Allowable Emissions Comment (Description of Operating Method):		
Allowable Emissions Allowable Emissions _ o	of	
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:	
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year	
5. Method of Compliance:	· · · · · · · · · · · · · · · · · · ·	
6. Allowable Emissions Comment (Description	of Operating Method):	

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### POLLUTANT DETAIL INFORMATION Page [5] of [12]

## F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     PM	2. Total Percent Efficiency of Control:
3. Potential Emissions:	4. Synthetically Limited?
0.11 lb/hour 0.0	1 tons/year Yes x No
5. Range of Estimated Fugitive Emissions (as	applicable):
to tons/year	
6. Emission Factor:	7. Emissions
	Method Code:
Reference: Vendor Data	5
8. Calculation of Emissions:	
Potential emissions are based on vendor dat	
The maximum hourly PM emission rate is 0	
_	ons are based on operating 200 hours per year.
Annual emissions = 0.11 lb/hr x 200 hours/	year x 1 ton/2,000 lb = 0.01 tons/year
·	
	•
9. Pollutant Potential/Estimated Fugitive Emis	ssions Comment:
The potential emissions are estimates based	
emissions are given for informational purpo	
	•

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## POLLUTANT DETAIL INFORMATION Page [6] of [12]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions	of		
1. Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:  lb/hour tons/year		
5. Method of Compliance:			
6. Allowable Emissions Comment (Description of Operating Method):			
Allowable Emissions Allowable Emissions	of		
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
<ul><li>5. Method of Compliance:</li><li>6. Allowable Emissions Comment (Description of Operating Method):</li></ul>			
Allowable Emissions Allowable Emissions			
Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5. Method of Compliance:			
6. Allowable Emissions Comment (Descrip	otion of Operating Method):		

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### POLLUTANT DETAIL INFORMATION Page [7] of [12]

## F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1. Pollutant Emitted: PM10	2. Total Percent Efficiency of Control:
3. Potential Emissions:	4. Synthetically Limited?
	1 tons/year Yes x No
5. Range of Estimated Fugitive Emissions (as to tons/year	applicable):
6. Emission Factor:	7. Emissions
	Method Code:
Reference: Vendor Data	5
8. Calculation of Emissions: Potential emissions are based on vendor dat. The maximum hourly PM ₁₀ emission rate is The maximum annual potential PM ₁₀ emissions = 0.11 lb/hr x 200 hours/y	ons are based on operating 200 hours per year.
9. Pollutant Potential/Estimated Fugitive Emissions Comment: The potential emissions are estimates based on preliminary vendor data. The potential emissions are given for informational purposes and do not represent limits.	

## POLLUTANT DETAIL INFORMATION Page [8] of [12]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions	of			
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year			
5. Method of Compliance:				
6. Allowable Emissions Comment (Description of Operating Method):				
Allowable Emissions	of			
Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year			
Method of Compliance:      Allowable Emissions Comment (Description of Operating Method):				
Allowable Emissions Allowable Emissions	of			
Basis for Allowable Emissions Code:	Emissions:  2. Future Effective Date of Allowable  Emissions:			
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year			
5. Method of Compliance:				
6. Allowable Emissions Comment (Description	n of Operating Method):			

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#### POLLUTANT DETAIL INFORMATION Page [9] of [12]

### F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION -POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     SO2	2. Total Percent Efficiency of Control:
3. Potential Emissions: 0.003 lb/hour 0.0003	4. Synthetically Limited?  Yes X No
5. Range of Estimated Fugitive Emissions (as to tons/year	applicable):
6. Emission Factor:  Reference: Vendor Data	7. Emissions Method Code: 5
8. Calculation of Emissions: Potential emissions are based on vendor data using fuel oil with 0.0015 percent sulfur content. The maximum hourly SO ₂ emission rate is 0.003 lb/hour. The maximum annual potential SO ₂ emissions are based on operating 200 hours per year. Annual emissions = 0.003 lb/hr x 200 hours/year x 1 ton/2,000 lb = 0.0003 tons/year	
9. Pollutant Potential/Estimated Fugitive Emissions Comment: Potential emissions shown in Fields 3 and 8 are based on using fuel oil with 0.0015 percent sulfur content. The potential emissions are estimates based on preliminary vendor data. The potential emissions are given for informational purposes and do not represent limits.	

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### POLLUTANT DETAIL INFORMATION Page [10] of [12]

## F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions _ o	of
Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	Equivalent Allowable Emissions:     lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description	of Operating Method):
Allowable Emissions Allowable Emissions _ o	of _
Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description	of Operating Method):

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POLLUTANT DETAIL INFORMATION
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### F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     VOC	2. Total Percent Effici	ency of Control:		
3. Potential Emissions:	4. Synt	hetically Limited?		
0.21 lb/hour 0.02	2 tons/year	Yes x No		
5. Range of Estimated Fugitive Emissions (as	applicable):			
to tons/year				
6. Emission Factor:		7. Emissions		
		Method Code:		
Reference: Vendor Data		5		
8. Calculation of Emissions:				
Potential emissions are based on vendor dat	a.			
The maximum hourly VOC emission rate is	0.21 lb/hour.			
The maximum annual potential VOC emissions are based on operating 200 hours per year.				
Annual emissions = $0.21 \text{ lb/hr} \times 200 \text{ hours/year} \times 1 \text{ ton/2,000 lbs} = 0.02 \text{ tons/year}$				
	• 0			
	9. Pollutant Potential/Estimated Fugitive Emissions Comment:			
•	The potential emissions are estimates based on preliminary vendor data. The potential			
emissions are given for informational purpo	ses and do not represent	iimits.		

### POLLUTANT DETAIL INFORMATION Page [12] of [12]

### F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions	of
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description	n of Operating Method):
Allowable Emissions Allowable Emissions	of
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
<ul><li>5. Method of Compliance:</li><li>6. Allowable Emissions Comment (Description)</li></ul>	n of Operating Method):
Allowable Emissions Allowable Emissions	of
Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description	on of Operating Method):

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#### G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

	sible Emissions Limitation: Visil	Di Diiii	v	•
1.	Visible Emissions Subtype:		2. Basis for Allowable	Opacity:
			Rule	Other
3.	Allowable Opacity:			
			cceptional Conditions:	%
	Maximum Period of Excess Opac	ity Allowe	ed:	min/hour
4.	Method of Compliance:			
5.	Visible Emissions Comment:			
<u>Vi</u>	sible Emissions Limitation: Visil	ble Emissi	ons Limitation of	
	Visible Emissions Subtype:	ble Emissi	ons Limitation of	Opacity:
_		ble Emissi		Opacity:
	Visible Emissions Subtype:  Allowable Opacity:		2. Basis for Allowable Rule	Other
1.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions:	% Ех	2. Basis for Allowable Rule	Other %
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac	% Ех	2. Basis for Allowable Rule	Other
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions:	% Ех	2. Basis for Allowable Rule	Other %
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac	% Ех	2. Basis for Allowable Rule	Other %
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac	% Ех	2. Basis for Allowable Rule	Other %
1.     3.     4.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac Method of Compliance:	% Ех	2. Basis for Allowable Rule	Other %
1.       3.       4.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac Method of Compliance:	% Ех	2. Basis for Allowable Rule	Other %
1.       3.       4.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac Method of Compliance:	% Ех	2. Basis for Allowable Rule	Other %
1.       3.       4.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: Maximum Period of Excess Opac Method of Compliance:	% Ех	2. Basis for Allowable Rule	Other %

#### H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

Continuous Monitoring System: Continuous Monitor of _

1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	☐ Rule ☐ Other
4.	Monitor Information Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
Co	ontinuous Monitoring System: Continuous	Monitor _ of _
1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	Rule Other
4.	Monitor Information  Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
	·	

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#### **EMISSIONS UNIT INFORMATION**

Section [3]

of [6]

#### I. EMISSIONS UNIT ADDITIONAL INFORMATION

#### Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID: Previously Submitted, Date
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)    Attached, Document ID: Attach. L Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID: Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID: Previously Submitted, Date Not Applicable (construction application)
5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)   X Attached, Document ID: Attach. O Previously Submitted, Date  Not Applicable
6.	Compliance Demonstration Reports/Records  Attached, Document ID:  Test Date(s)/Pollutant(s) Tested:
	Previously Submitted, Date:  Test Date(s)/Pollutant(s) Tested:
	To be Submitted, Date (if known):  Test Date(s)/Pollutant(s) Tested:
	× Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute  Attached, Document ID: Not Applicable

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### **EMISSIONS UNIT INFORMATION**

Section [3] of [6]

#### Additional Requirements for Air Construction Permit Applications

Additional Regardements for All Construction I crimit Applications
1. Control Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7), F.A.C.; 40 CFR 63.43(d) and (e))
x Attached, Document ID: Attach. P Not Applicable
2. Good Engineering Practice Stack Height Analysis (Rule 62-212.400(5)(h)6., F.A.C., and
Rule 62-212.500(4)(f), F.A.C.)
x Attached, Document ID: Attach. Q Not Applicable
3. Description of Stack Sampling Facilities (Required for proposed new stack sampling facilities only)
Attached, Document ID: Not Applicable
Additional Requirements for Title V Air Operation Permit Applications
1. Identification of Applicable Requirements
Attached, Document ID:
2. Compliance Assurance Monitoring
Attached, Document ID: Not Applicable
3. Alternative Methods of Operation
Attached, Document ID: Not Applicable
4. Alternative Modes of Operation (Emissions Trading)
Attached, Document ID: Not Applicable
5. Acid Rain Part Application
Certificate of Representation (EPA Form No. 7610-1)
Copy Attached, Document ID:
Acid Rain Part (Form No. 62-210.900(1)(a))
Attached, Document ID:
☐ Previously Submitted, Date: Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
Attached, Document ID:
Previously Submitted, Date:
New Unit Exemption (Form No. 62-210.900(1)(a)2.)
Attached, Document ID:
Previously Submitted, Date:
Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)
Attached, Document ID:
Previously Submitted, Date:
Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)
Attached, Document ID:
Previously Submitted, Date:
Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)
Attached, Document ID:
Previously Submitted, Date:
Not Applicable

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Additional Requirem	ents Comment		
}			
}			

Effective: 06/16/03

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# EMISSIONS UNIT INFORMATION Section [4] of [6] III. EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Application - For Title V air operation permitting only, emissions units are classified as regulated, unregulated, or insignificant. If this is an application for Title V air operation permit, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each regulated and unregulated emissions unit addressed in this application for air permit. Some of the subsections comprising the Emissions Unit Information Section of the form are optional for unregulated emissions units. Each such subsection is appropriately marked. Insignificant emissions units are required to be listed at Section II, Subsection C.

Air Construction Permit or FESOP Application - For air construction permitting or federally enforceable state air operation permitting, emissions units are classified as either subject to air permitting or exempt from air permitting. The concept of an "unregulated emissions unit" does not apply. If this is an application for air construction permit or FESOP, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air permitting are required to be listed at Section II, Subsection C.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit Application — Where this application is used to apply for both an air construction permit and a revised/renewal Title V air operation permit, each emissions unit is classified as either subject to air permitting or exempt from air permitting for air construction permitting purposes and as regulated, unregulated, or insignificant for Title V air operation permitting purposes. The air construction permitting classification must be used to complete the Emissions Unit Information Section of this application for air permit. A separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air construction permitting and insignificant emissions units are required to be listed at Section II, Subsection C.

If submitting the application form in hard copy, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application must be indicated in the space provided at the top of each page.

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#### **EMISSIONS UNIT INFORMATION**

Section [4]

of [6]

#### A. GENERAL EMISSIONS UNIT INFORMATION

#### Title V Air Operation Permit Emissions Unit Classification

	renewal T	1. Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)				
	emission  The en	<ul> <li>The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.</li> <li>The emissions unit addressed in this Emissions Unit Information Section is an</li> </ul>				
Į		ated emissions unit.	atus			
ſ				n. (Chaak ana)		
	x The single and w	missions Unit Addressed is Emissions Unit Information unit Information has at least one descriptions Unit Information or production units are	rmation Section unit, or activity, finable emission tion Section add	addresses, as a single which produces one of a point (stack or vent). dresses, as a single em	or more air pollutants issions unit, a group of	
۱		or vent) but may also p			<b>,</b>	
	_	Emissions Unit Information or process or production u			_	
	2. Description	on of Emissions Unit A	ddressed in this	Section: Safe Shutdo	own Generator.	
	3. Emissions	Unit Identification Nu	mber:			
	4. Emissions Unit Statu Code: C		6. Initial Startup Date:	7. Emissions Unit Major Group SIC Code: 49	8. Acid Rain Unit?  Yes  No	
	9. Package U Manufact	Jnit: urer: TBD		Model Number: TBI	)	
l		r Nameplate Rating:				
		Unit Comment:				
١						

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### **Emissions Unit Control Equipment**

Control Equipment/Method(s) Description:	
	•
2. Control Device or Method Code(s):	

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#### **B. EMISSIONS UNIT CAPACITY INFORMATION**

(Optional for unregulated emissions units.)

#### **Emissions Unit Operating Capacity and Schedule**

1.	Maximum Process or Throughput Rate:	
2.	Maximum Production Rate: 765 HP (approximate)	
3.	Maximum Heat Input Rate:	
4.	Maximum Incineration Rate: pounds/hr	
	tons/day	
5.	Requested Maximum Operating Schedule:	
	24 hours/day	7 days/week
	52 weeks/year	8,760 hours/year

6. Operating Capacity/Schedule Comment: It is conservatively estimated that the safe shutdown generator will operate approximately 200 hours per year. Because this is emergency equipment, a maximum operating schedule is not requested. Because a specific manufacturer and model has not been determined, the maximum production rate provided is an approximate value.

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## C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

### **Emission Point Description and Type**

1. Identification of Point on	Plot Plan or	2. Emission Point T	Type Code:
Flow Diagram: Safe Shute	lown Generator	1	
3. Descriptions of Emission			
<ul><li>4. ID Numbers or Descriptio</li><li>5. Discharge Type Code:</li></ul>	6. Stack Height		7. Exit Diameter:
V	11 feet		0.665 feet
8. Exit Temperature: 981°F			10. Water Vapor: %
11. Maximum Dry Standard F dscfm	low Rate:	12. Nonstack Emissi	on Point Height:
13. Emission Point UTM Coordinates  Zone: 17 East (km): 561.5347  North (km): 3028 9730		14. Emission Point Latitude/Longitude Latitude (DD/MM/SS) Longitude (DD/MM/SS)	

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### D. SEGMENT (PROCESS/FUEL) INFORMATION

### **Segment Description and Rate:** Segment <u>1</u> of <u>1</u>

1.	Fuel oil used in the safe shutdown generator				
				,	
2.	Source Classification Code (SCC): 20100301		3. SCC Units: Thousand Gallons Burned		
4.	Maximum Hourly Rate: 0.0363	5. Maximum 7.26	Annual Rate:	6. Estimated Annual Activity Factor:	
7.	Maximum % Sulfur:	8. Maximum	% Ash:	9. Million Btu per SCC Unit: 137 (HHV)	
10.	10. Segment Comment: The above information is based on preliminary vendor information and represents the expected approximate emission unit parameters. The annual rate is based on an estimated 200 hours per year of operation.				
Se	gment Description and Ra		of _		
1.	1. Segment Description (Process/Fuel Type):				
2.	Source Classification Code	e (SCC):	3. SCC Units:		
4.	Maximum Hourly Rate:	5. Maximum	Annual Rate:	6. Estimated Annual Activity Factor:	
7.	Maximum % Sulfur:	8. Maximum	% Ash:	9. Million Btu per SCC Unit:	
10.	. Segment Comment:	1			

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#### E. EMISSIONS UNIT POLLUTANTS

#### List of Pollutants Emitted by Emissions Unit

1. Pollutant Emitted	2. Primary Control Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
со			NS
NOX			NS
PM		·	NS
PM10			NS
SO2			NS
VOC			NS
			-
	·		
		<u> </u>	

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### POLLUTANT DETAIL INFORMATION [1] of [12]

### F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1. Pollutant Emitted:	2. Total Percent Efficiency of Control:		
CO			
3. Potential Emissions:	4. Synthetically Limited?		
0.89 lb/hour 0.0	9 tons/year Yes x No		
5. Range of Estimated Fugitive Emissions (as	applicable):		
to tons/year			
6. Emission Factor:	7. Emissions		
	Method Code:		
Reference: Vendor Data	5		
8. Calculation of Emissions:			
Potential emissions are based on vendor da	ta.		
The maximum hourly CO emission rate is	).89 lb/hour.		
<u>-</u>	ons are based on operating 200 hours per year.		
Annual emissions = $0.89 \text{ lb/hr} \times 200 \text{ hours/year} \times 1 \text{ ton/2,000 lb} = 0.09 \text{ tons/year}$			
·			
O. Pallutant Patential/Estimated Engitive Emi	orione Comment		
9. Pollutant Potential/Estimated Fugitive Emissions Comment:  The notential emissions are estimated based on maliminary yander date. The notential			
The potential emissions are estimates based on preliminary vendor data. The potential emissions are given for informational purposes and do not represent limits.			
cinissions are given for informational purpo	ises and do not represent mints.		
I .			

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### POLLUTANT DETAIL INFORMATION Page [2] of [12]

### F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

<u>Ai</u>	lowable Emissions Allowable Emissions	of_	<del>_</del>		
1.	Basis for Allowable Emissions Code:	2.	2. Future Effective Date of Allowable Emissions:		
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions:		
			lb/hour tons/year		
5.	Method of Compliance:				
6.	Allowable Emissions Comment (Description	of	Operating Method):		
L			<del>-</del> .		
Al	lowable Emissions Allowable Emissions				
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable		
		ļ.,	Emissions:		
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions:		
			lb/hour tons/year		
5.	Method of Compliance:		•		
<u> </u>					
6.	Allowable Emissions Comment (Description	101	Operating Method):		
_		of_	<del>_</del>		
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable		
			Emissions:		
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions:		
			lb/hour tons/year		
5.	Method of Compliance:		1000		
6.	6. Allowable Emissions Comment (Description of Operating Method):				

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POLLUTANT DETAIL INFORMATION
Page [3] of [12]

### F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted:	2. Total Perce	ent Efficie	ency of Control:	
	NOX				
3.	Potential Emissions:		4. Synth	etically Limited?	
	11.3 lb/hour 1.13	3 tons/year		es x No	
5.	Range of Estimated Fugitive Emissions (as	applicable):			
	to tons/year				
6.	Emission Factor:			7. Emissions	
				Method Code:	
	Reference: Vendor Data			5	
8.	Calculation of Emissions:				
1	Potential emissions are based on vendor data	a.			
	The maximum hourly NO _x emission rate is 11.3 lb/hour.				
	The maximum annual potential NO _x emissions are based on operating 200 hours per year.				
	Annual emissions = $11.3 \text{ lb/hr} \times 200 \text{ hours/year} \times 1 \text{ ton/2,000 lb} = 1.13 \text{ tons/year}$				
9.	Pollutant Potential/Estimated Fugitive Emis				
	The potential emissions are estimates based on preliminary vendor data. The potential				
	emissions are given for informational purposes and do not represent limits.				
1					

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### POLLUTANT DETAIL INFORMATION Page [4] of [12]

### F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions _ of _				
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year			
5. Method of Compliance:				
6. Allowable Emissions Comment (Description of Operating Method):				

#### Allowable Emissions Allowable Emissions of

Allowable Emissions 1 Movacle Emissions 01				
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:			
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:			
	lb/hour tons/year			
5. Method of Compliance:				
6. Allowable Emissions Comment (Description	of Operating Method):			

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POLLUTANT DETAIL INFORMATION
Page [5] of [12]

### F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     PM	2. Total Percent Efficiency of Control:		
3. Potential Emissions:	4. Synthetically Limited?		
0.08 lb/hour 0.0	1 tons/year Yes x No		
5. Range of Estimated Fugitive Emissions (as	s applicable):		
to tons/year			
6. Emission Factor:	7. Emissions		
	Method Code:		
Reference: Vendor Data	5		
8. Calculation of Emissions:			
Potential emissions are based on vendor da	ta.		
The maximum hourly PM emission rate is			
<u>-</u>	ons are based on operating 200 hours per year.		
Annual emissions = $0.08 \text{ lb/hr} \times 200 \text{ hours/year} \times 1 \text{ ton/2,000 lb} = 0.01 \text{ tons/year}$			
·			
9. Pollutant Potential/Estimated Fugitive Emi	ssions Comment:		
9. Pollutant Potential/Estimated Fugitive Emissions Comment: The potential emissions are estimates based on preliminary vendor data. The potential			
<u>-</u>	emissions are given for informational purposes and do not represent limits.		
parp.	nor represent imme.		

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### POLLUTANT DETAIL INFORMATION Page [6] of [12]

### F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions	_ of		
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5. Method of Compliance:			
6. Allowable Emissions Comment (Description	• • • • • • • • • • • • • • • • • • •		
Allowable Emissions Allowable Emissions			
Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
Method of Compliance:      Allowable Emissions Comment (Description of Operating Method):			
Allowable Emissions Allowable Emissions	of		
Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5. Method of Compliance:			
6. Allowable Emissions Comment (Description	on of Operating Method):		

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POLLUTANT DETAIL INFORMATION
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### F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

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Allowable Emissions Allowable Emissions

### POLLUTANT DETAIL INFORMATION Page [8] of [12]

### F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

of

Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:		
	lb/hour tons/year		
5. Method of Compliance:			
6. Allowable Emissions Comment (Description			
Allowable Emissions	_ of		
Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:		
	lb/hour tons/year		
<ul><li>5. Method of Compliance:</li><li>6. Allowable Emissions Comment (Description)</li></ul>	n of Operating Method):		
Allowable Emissions Allowable Emissions	of		
Basis for Allowable Emissions Code:	Emissions:  2. Future Effective Date of Allowable  Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5. Method of Compliance:			
6. Allowable Emissions Comment (Description of Operating Method):			

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POLLUTANT DETAIL INFORMATION
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### F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1. Pollutant Emitted: SO2	2. Total Percent Efficience	cy of Control:			
3. Potential Emissions:	4. Synthet	tically Limited?			
0.008 lb/hour 0.00	l tons/year	s x No			
5. Range of Estimated Fugitive Emissions (as	applicable):				
to tons/year					
6. Emission Factor:	7	7. Emissions			
		Method Code:			
Reference: Vendor Data		5			
8. Calculation of Emissions:					
Potential emissions are based on vendor dat content.	Potential emissions are based on vendor data using fuel oil with 0.0015 percent sulfur content.				
The maximum hourly SO ₂ emission rate is 0	).008 lb/hour.				
The maximum annual potential $SO_2$ emissions are based on operating 200 hours per year. Annual emissions = 0.008 lb/hr x 200 hours/year x 1 ton/2,000 lb = 0.001 tons/year					
9. Pollutant Potential/Estimated Fugitive Emissions Comment:					
	Potential emissions shown in Fields 3 and 8 are based on using fuel oil with 0.0015 percent				
<u>-</u>	sulfur content. The potential emissions are estimates based on preliminary vendor data.				
The potential emissions are given for inform	national purposes and do no	of represent limits.			

### POLLUTANT DETAIL INFORMATION Page [10] of [12]

### F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions _ o	of	
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:	
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:	
	lb/hour tons/year	
5. Method of Compliance:		
6. Allowable Emissions Comment (Description	of Operating Method):	
Allowable Emissions Allowable Emissions _ o	of_	
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:	
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year	
5. Method of Compliance:		
6. Allowable Emissions Comment (Description	of Operating Method):	

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POLLUTANT DETAIL INFORMATION
Page [11] of [12]

### F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     VOC	2. Total Percent Efficiency of Control:	
3. Potential Emissions:	4. Synthetically Limited?	
0.11 lb/hour 0.01	tons/year Yes x No	
5. Range of Estimated Fugitive Emissions (as	applicable):	
to tons/year		
6. Emission Factor:	7. Emissions	
	Method Code:	
Reference: Vendor Data	5	
Annual emissions = 0.11 lb/hr x 200 hours/	0.11 lb/hour. ions are based on operating 200 hours per year. year x 1 ton/2,000 lbs = 0.01 tons/year	
<ol> <li>Pollutant Potential/Estimated Fugitive Emissions Comment:         The potential emissions are estimates based on preliminary vendor data. The potential emissions are given for informational purposes and do not represent limits.     </li> </ol>		

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Allowable Emissions __ of ___

### POLLUTANT DETAIL INFORMATION Page [12] of [12]

### F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5. Method of Compliance:			
6. Allowable Emissions Comment (Description	n of Operating Method):		
Allowable Emissions Allowable Emissions	_ of		
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5. Method of Compliance:			
6. Allowable Emissions Comment (Description			
Allowable Emissions Allowable Emissions	_ of		
Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:		
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year		
5. Method of Compliance:			
6. Allowable Emissions Comment (Description	n of Operating Method):		

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#### G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

Visible Emissions Limitation: Visible Emissions Limitation of				
1.	Visible Emissions Subtype:	2. Basis for Allowable Opacity:		
		Rule Other		
3.	Allowable Opacity:			
		xceptional Conditions:		
	Maximum Period of Excess Opacity Allow	red: min/hour		
4.	Method of Compliance:			
5.	Visible Emissions Comment:			
Visible Emissions Limitation: Visible Emissions Limitation of				
<u>Vi</u>	sible Emissions Limitation: Visible Emiss	ions Limitation of		
_	sible Emissions Limitation: Visible Emiss  Visible Emissions Subtype:	2. Basis for Allowable Opacity:		
1.	Visible Emissions Subtype:			
1.	Visible Emissions Subtype:  Allowable Opacity:	2. Basis for Allowable Opacity:  Rule  Other		
1.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % E	2. Basis for Allowable Opacity:  Rule  Other  conditions: %		
3.	Visible Emissions Subtype:  Allowable Opacity:  Normal Conditions: % E  Maximum Period of Excess Opacity Allow	2. Basis for Allowable Opacity:  Rule  Other  conditions: %		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % E	2. Basis for Allowable Opacity:  Rule  Other  conditions: %		
3.	Visible Emissions Subtype:  Allowable Opacity:  Normal Conditions: % E  Maximum Period of Excess Opacity Allow	2. Basis for Allowable Opacity:  Rule  Other  conditions: %		
3.	Visible Emissions Subtype:  Allowable Opacity:  Normal Conditions: % E  Maximum Period of Excess Opacity Allow	2. Basis for Allowable Opacity:  Rule  Other  conditions: %		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % E Maximum Period of Excess Opacity Allow Method of Compliance:	2. Basis for Allowable Opacity:  Rule  Other  conditions: %		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % E Maximum Period of Excess Opacity Allow Method of Compliance:	2. Basis for Allowable Opacity:  Rule  Other  conditions: %		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % E Maximum Period of Excess Opacity Allow Method of Compliance:	2. Basis for Allowable Opacity:  Rule  Other  conditions: %		
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % E Maximum Period of Excess Opacity Allow Method of Compliance:	2. Basis for Allowable Opacity:  Rule  Other  conditions: %		

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#### H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

<u>Continuous Monitoring System:</u> Continuous Monitor _ of _

1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	☐ Rule ☐ Other
4.	Monitor Information Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
Co	ntinuous Monitoring System: Continuous	Monitor _ of _
1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	Rule Other
4.	Monitor Information Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	•

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#### I. EMISSIONS UNIT ADDITIONAL INFORMATION

#### Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID: Previously Submitted, Date
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)            x         Attached, Document ID: Attach. L         Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID: Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID:  Previously Submitted, Date  Not Applicable (construction application)
5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  X Attached, Document ID: Attach. O Previously Submitted, Date  Not Applicable
6.	Compliance Demonstration Reports/Records  Attached, Document ID:  Test Date(s)/Pollutant(s) Tested:
	Previously Submitted, Date:  Test Date(s)/Pollutant(s) Tested:
	To be Submitted, Date (if known):  Test Date(s)/Pollutant(s) Tested:
	× Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute  Attached, Document ID: x Not Applicable

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Additional Requirements for Air Construction Permit Applications
1. Control Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7),
F.A.C.; 40 CFR 63.43(d) and (e))  x Attached, Document ID: Attach. P Not Applicable
2. Good Engineering Practice Stack Height Analysis (Rule 62-212.400(5)(h)6., F.A.C., and Rule 62-212.500(4)(f), F.A.C.)
x Attached, Document ID: Attach. Q Not Applicable
3. Description of Stack Sampling Facilities (Required for proposed new stack sampling facilities only)
Attached, Document ID: × Not Applicable
Additional Requirements for Title V Air Operation Permit Applications
1. Identification of Applicable Requirements
Attached, Document ID:
2. Compliance Assurance Monitoring
Attached, Document ID: Not Applicable
3. Alternative Methods of Operation
Attached, Document ID: Not Applicable
4. Alternative Modes of Operation (Emissions Trading)
Attached, Document ID: Not Applicable
5. Acid Rain Part Application
Certificate of Representation (EPA Form No. 7610-1)
Copy Attached, Document ID:
☐ Acid Rain Part (Form No. 62-210.900(1)(a))
Attached, Document ID:
Previously Submitted, Date:
Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
Attached, Document ID:
Previously Submitted, Date:
☐ New Unit Exemption (Form No. 62-210.900(1)(a)2.)
Attached, Document ID:
Previously Submitted, Date:
Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)
Attached, Document ID:
Previously Submitted, Date:
Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)
Attached, Document ID:
Previously Submitted, Date:
Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)
Attached, Document ID:
Previously Submitted, Date:
☐ Not Applicable

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<b>Additional Requirements Comment</b>	
·	
·	·

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#### III. EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Application - For Title V air operation permitting only, emissions units are classified as regulated, unregulated, or insignificant. If this is an application for Title V air operation permit, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each regulated and unregulated emissions unit addressed in this application for air permit. Some of the subsections comprising the Emissions Unit Information Section of the form are optional for unregulated emissions units. Each such subsection is appropriately marked. Insignificant emissions units are required to be listed at Section II, Subsection C.

Air Construction Permit or FESOP Application - For air construction permitting or federally enforceable state air operation permitting, emissions units are classified as either subject to air permitting or exempt from air permitting. The concept of an "unregulated emissions unit" does not apply. If this is an application for air construction permit or FESOP, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air permitting are required to be listed at Section II, Subsection C.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit Application — Where this application is used to apply for both an air construction permit and a revised/renewal Title V air operation permit, each emissions unit is classified as either subject to air permitting or exempt from air permitting for air construction permitting purposes and as regulated, unregulated, or insignificant for Title V air operation permitting purposes. The air construction permitting classification must be used to complete the Emissions Unit Information Section of this application for air permit. A separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air construction permitting and insignificant emissions units are required to be listed at Section II, Subsection C.

If submitting the application form in hard copy, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application must be indicated in the space provided at the top of each page.

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#### **EMISSIONS UNIT INFORMATION**

Section [5]

of [6]

#### A. GENERAL EMISSIONS UNIT INFORMATION

#### **Title V Air Operation Permit Emissions Unit Classification**

re	1. Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)				
_	<ul> <li>☐ The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.</li> <li>☐ The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.</li> </ul>				
<u>Emiss</u>	sions Unit	Description and Sta	<u>itus</u>		
1. Ty	ype of Emis	ssions Unit Addresse	d in this Section	on: (Check one)	
	This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).				•
	This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.				
	This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only.				
2. Description of Emissions Unit Addressed in this Section: Fuel Oil Storage Tank.					
3. Er	missions U	nit Identification Nur	mber:	_	
	missions nit Status	5. Commence Construction	6. Initial Startup	7. Emissions Unit Major Group	8. Acid Rain Unit?
	ode:	Date:	Date:	SIC Code:	× No
	ackage Unit			Model Number:	<u> </u>
10. C	Generator N	ameplate Rating:			
11. Emissions Unit Comment: The capacity of the Fuel Oil Storage Tank is slightly less than 990,000 gallons. In accordance with Rule 62-210.300(3)(b)1., F.A.C., the fuel oil storage tank is exempt from the requirement to obtain an air construction permit. However, the fuel oil storage tank VOC emissions were included in the Project potential to emit estimates and this Emissions Unit Information section is used to provide information on the fuel oil storage tank.					

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### **Emissions Unit Control Equipment**

1.	Control Equipment/Method(s) Description:
2	Control Device or Method Code(s):

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#### **B. EMISSIONS UNIT CAPACITY INFORMATION**

(Optional for unregulated emissions units.)

#### **Emissions Unit Operating Capacity and Schedule**

1.	Maximum Process or Throughput Rate: 6,850,000 gallons per year	
2.	Maximum Production Rate:	
3.	Maximum Heat Input Rate:	
4.	Maximum Incineration Rate: pounds/hr	
	tons/day	
5.	Requested Maximum Operating Schedule:	
	24 hours/day	7 days/week
	52 weeks/year	8,760 hours/year
6.	Operating Capacity/Schedule Comment:	
'		

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#### **EMISSIONS UNIT INFORMATION** Section [5] [6] of

### C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

### **Emission Point Description and Type**

	2. Emission Point 7	Type Code:
ssion Points Comprising	g this Emissions Unit	for VE Tracking. Fuel
criptions of Emission Ur	nits with this Emission	n Point in Common:
de: 6. Stack Height	:	7. Exit Diameter:
9. Actual Volume	metric Flow Rate:	10. Water Vapor: %
dard Flow Rate:	12. Nonstack Emiss 40 ft	ion Point Height:
(km): 561.8163	14. Emission Point I Latitude (DD/M Longitude (DD/I	,
• •	Zongawa (22)	
	criptions of Emission Under the decimal section of Emission Under the decimal section Under the	de: 6. Stack Height:  9. Actual Volumetric Flow Rate: acfm dard Flow Rate: 12. Nonstack Emiss: 40 ft M Coordinates (km): 561.8163 h (km): 3028.9551 Longitude (DD/M)

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### D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment Description and Rate: Segment 1 of 2

1.	Segment Description (Process/Fuel Type):     Breathing loss					
2.	Source Classification Code 2501000090	e (S	CC):	3. SCC Units: Thousand C		ons Stored
4.	Maximum Hourly Rate:	5.	Maximum . 0	Annual Rate:	6.	Estimated Annual Activity Factor: 1,000
7.	Maximum % Sulfur:	8.	Maximum	% Ash:	9.	Million Btu per SCC Unit:
10.	Segment Comment:					
L						-
Se	gment Description and Ra	te:	Segment 2	_ of <u>_2</u>		
1.	Segment Description (Proc Working loss	cess	/Fuel Type):			-
	Working 1033					
2.	Source Classification Code	e (S	CC):	3. SCC Units:		
L_	2501000090				_	ons Transferred or Handled
4.	Maximum Hourly Rate:	5.	Maximum 6,850	Annual Rate:	6.	Estimated Annual Activity Factor:
7.	Maximum % Sulfur:	8.	Maximum	% Ash:	9.	Million Btu per SCC Unit:
10.	Segment Comment:		_			

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### E. EMISSIONS UNIT POLLUTANTS

### List of Pollutants Emitted by Emissions Unit

1.	Pollutant Emitted	Primary Control     Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
	voc			NS
			_	
	<u> </u>			
			_	
				_

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POLLUTANT DETAIL INFORMATION
Page [1] of [2]

## F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

Pollutant Emitted:     VOC	2. Total Percent Efficiency of Control:
3. Potential Emissions: 0.04 lb/hour 0.16	4. Synthetically Limited?  Stons/year Yes x No
5. Range of Estimated Fugitive Emissions (as to tons/year	applicable):
6. Emission Factor:  Reference: USEPA TANKS Program	7. Emissions Method Code: 3
8. Calculation of Emissions: Potential emissions are based on use of the The maximum annual VOC emission rate is The TANKS program gives the VOC emiss The annual emissions were spread out evenl value. The hourly VOC emission rate is 0.04 lb/ho	323.1 lb/year = 0.16 tons/year. ions in lbs per year rather than lbs per hour. y over the entire year to obtain a lbs per hour
9. Pollutant Potential/Estimated Fugitive Emis	sions Comment:

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## POLLUTANT DETAIL INFORMATION Page [2] of [2]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions	_ of
1. Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:
	lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description  Allowable Emissions Allowable Emissions	
Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
Method of Compliance:      Allowable Emissions Comment (Description)	on of Operating Method):
Allowable Emissions Allowable Emissions	of
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable
1. Basis for Allowable Emissions Code:	Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:  lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description	on of Operating Method):

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#### G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

<u>Vi</u>	Visible Emissions Limitation: Visible Emissions Limitation of				
1.	Visible Emissions Subtype:	2. Basis for Allowable Opacity:			
		Rule Other			
3.	Allowable Opacity:				
	Normal Conditions: %	Exceptional Conditions: %			
	Maximum Period of Excess Opacity Allo	owed: min/hour			
4.	Method of Compliance:				
5.	Visible Emissions Comment:				
ا.	Visible Emissions Comment.				
		·			
1					
<u>Vi</u>	sible Emissions Limitation: Visible Em	issions Limitation of			
	sible Emissions Limitation: Visible Emissions Subtype:	issions Limitation of 2. Basis for Allowable Opacity:			
1.		2. Basis for Allowable Opacity:			
1.	Visible Emissions Subtype:	2. Basis for Allowable Opacity:			
1.	Visible Emissions Subtype:  Allowable Opacity:	2. Basis for Allowable Opacity:  Rule  Other  Exceptional Conditions: %			
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: %	2. Basis for Allowable Opacity:  Rule  Other  Exceptional Conditions: %			
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Maximum Period of Excess Opacity Allo	2. Basis for Allowable Opacity:  Rule  Other  Exceptional Conditions: %			
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Maximum Period of Excess Opacity Allo Method of Compliance:	2. Basis for Allowable Opacity:  Rule  Other  Exceptional Conditions: %			
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Maximum Period of Excess Opacity Allo	2. Basis for Allowable Opacity:  Rule  Other  Exceptional Conditions: %			
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Maximum Period of Excess Opacity Allo Method of Compliance:	2. Basis for Allowable Opacity:  Rule  Other  Exceptional Conditions: %			
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Maximum Period of Excess Opacity Allo Method of Compliance:	2. Basis for Allowable Opacity:  Rule  Other  Exceptional Conditions: %			
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Maximum Period of Excess Opacity Allo Method of Compliance:	2. Basis for Allowable Opacity:  Rule  Other  Exceptional Conditions: %			
3.	Visible Emissions Subtype:  Allowable Opacity: Normal Conditions: % Maximum Period of Excess Opacity Allo Method of Compliance:	2. Basis for Allowable Opacity:  Rule  Other  Exceptional Conditions: %			

#### H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

Continuous Monitoring System: Continuous Monitor of

1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	Rule Other
4.	Monitor Information Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
Co	entinuous Monitoring System: Continuous	Monitor _ of _
1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	Rule Other
4.	Monitor Information Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	

### EMISSIONS UNIT INFORMATION

Section [5]

of [6]

### I. EMISSIONS UNIT ADDITIONAL INFORMATION

#### Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID: Previously Submitted, Date
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID: NA Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID: NA Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID:  Previously Submitted, Date  Not Applicable (construction application)
5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  X Attached, Document ID: Attach. O Previously Submitted, Date  Not Applicable
6.	Compliance Demonstration Reports/Records  Attached, Document ID:  Test Date(s)/Pollutant(s) Tested:
	Previously Submitted, Date:  Test Date(s)/Pollutant(s) Tested:
	To be Submitted, Date (if known):  Test Date(s)/Pollutant(s) Tested:
	× Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute  Attached, Document ID: Not Applicable

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#### **EMISSIONS UNIT INFORMATION**

Section [5] of [6]

#### **Additional Requirements for Air Construction Permit Applications**

1. Control Technology Review and Analy F.A.C.; 40 CFR 63.43(d) and (e))	ysis (Rules 62-212.400(6) and 62-212.500(7),
Attached, Document ID:	× Not Applicable
2. Good Engineering Practice Stack Heig	ht Analysis (Rule 62-212.400(5)(h)6., F.A.C., and
Rule 62-212.500(4)(f), F.A.C.)	
Attached, Document ID:	Not Applicable
	es (Required for proposed new stack sampling
facilities only)	
Attached, Document ID:	x Not Applicable
Additional Requirements for Title V Air	r Operation Permit Applications
1. Identification of Applicable Requirement	
Attached, Document ID:	
2. Compliance Assurance Monitoring	
Attached, Document ID:	Not Applicable
3. Alternative Methods of Operation	
Attached, Document ID:	Not Applicable
4. Alternative Modes of Operation (Emiss	<del>-</del>
Attached, Document ID:	Not Applicable
5. Acid Rain Part Application	
Certificate of Representation (EPA	
Copy Attached, Document ID	
Acid Rain Part (Form No. 62-210.9	* / * //
Attached, Document ID:	
Previously Submitted, Date:_	
Repowering Extension Plan (Form	* * * * * * * * * * * * * * * * * * * *
Attached, Document ID:	
Previously Submitted, Date:	**
New Unit Exemption (Form No. 62	
Attached, Document ID:	
Previously Submitted, Date:	
Retired Unit Exemption (Form No.	
Attached, Document ID: Previously Submitted, Date:	
Phase II NOx Compliance Plan (Fo	
Attached, Document ID:	
Previously Submitted, Date:	
Phase II NOx Averaging Plan (Form	
Previously Submitted, Date:	
Not Applicable	<del></del>

Additional R	<u>equirements Comm</u>	<u>ient</u>		

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#### III. EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Application - For Title V air operation permitting only, emissions units are classified as regulated, unregulated, or insignificant. If this is an application for Title V air operation permit, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each regulated and unregulated emissions unit addressed in this application for air permit. Some of the subsections comprising the Emissions Unit Information Section of the form are optional for unregulated emissions units. Each such subsection is appropriately marked. Insignificant emissions units are required to be listed at Section II, Subsection C.

Air Construction Permit or FESOP Application - For air construction permitting or federally enforceable state air operation permitting, emissions units are classified as either subject to air permitting or exempt from air permitting. The concept of an "unregulated emissions unit" does not apply. If this is an application for air construction permit or FESOP, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air permitting are required to be listed at Section II, Subsection C.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit Application -Where this application is used to apply for both an air construction permit and a revised/renewal Title V air operation permit, each emissions unit is classified as either subject to air permitting or exempt from air permitting for air construction permitting purposes and as regulated, unregulated, or insignificant for Title V air operation permitting purposes. The air construction permitting classification must be used to complete the Emissions Unit Information Section of this application for air permit. A separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air construction permitting and insignificant emissions units are required to be listed at Section II. Subsection C.

If submitting the application form in hard copy, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application must be indicated in the space provided at the top of each page.

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#### A. GENERAL EMISSIONS UNIT INFORMATION

#### Title V Air Operation Permit Emissions Unit Classification

1.	Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)							
	<ul> <li>☐ The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.</li> <li>☐ The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.</li> </ul>							
<u>E</u> :	missions Unit	Description and Sta	<u>itus</u>					
1.	Type of Emis	ssions Unit Addresse	d in this Section	n: (Check one)				
	process o		activity, which	lresses, as a single em produces one or more int (stack or vent).	, ,			
	process o		d activities whi	ich has at least one de	sissions unit, a group of finable emission point			
	<b></b>			addresses, as a single es which produce fug	e emissions unit, one or itive emissions only.			
2.	Description of	of Emissions Unit Ac	ldressed in this	Section: Mechanical	Draft Cooling Tower.			
	·							
3.	Emissions U	nit Identification Nur	mber:					
4.	Emissions Unit Status Code: C	5. Commence Construction Date:	6. Initial Startup Date:	7. Emissions Unit Major Group SIC Code: 49	8. Acid Rain Unit?  Yes  No			
9.	9. Package Unit: Manufacturer: Model Number:							
11	10. Generator Nameplate Rating:  11. Emissions Unit Comment:							
1								

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### **Emissions Unit Control Equipment**

1. Control Equipment/Method(s) Description: Drift eliminators	
·	
·	
2 Control Device or Method Code(s): 152	

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#### **B. EMISSIONS UNIT CAPACITY INFORMATION**

(Optional for unregulated emissions units.)

### **Emissions Unit Operating Capacity and Schedule**

1.	Maximum Process or Throughput Rate: 111,130 gpm design water flow	
2.	Maximum Production Rate:	
3.	Maximum Heat Input Rate:	
4.	Maximum Incineration Rate: pounds/hr	
	tons/day	
5.	Requested Maximum Operating Schedule:	
	24 hours/day 7 da	ys/week
	52 weeks/year 8,76	0 hours/year
6.	Operating Capacity/Schedule Comment:	

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## C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

### **Emission Point Description and Type**

1.	Identification of Point on I Flow Diagram: Cooling To		2.	Emission Point T	ype Code:
3.	Descriptions of Emission	Points Comprising	g thi	s Emissions Unit f	For VE Tracking:
4.	ID Numbers or Descriptio	ns of Emission Ur	its	with this Emission	Point in Common:
5.	Discharge Type Code: V	<ol><li>Stack Height 46 ft</li></ol>	:		7. Exit Diameter: 32 ft
8.	Exit Temperature: 95 F	9. Actual Volum 1,000,000 ac	umetric Flow Rate: 10. Water Vapor: %		-
11	. Maximum Dry Standard F dscfm	low Rate:	12	. Nonstack Emissi	on Point Height:
13	Emission Point UTM Coo Zone: 17 East (km): North (km)		14. Emission Point Latitude/Longitude Latitude (DD/MM/SS) Longitude (DD/MM/SS)		
15	Emission Point Comments tower. The information gi	The cooling tow		esign is an 8 cell r	nechanical draft cooling

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#### D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment Description and Rate: Segment 1 of 1

Segment Description     Drift loss	on (Process	/Fuel Type):			
2. Source Classificati 38500101	on Code (S	CC):	3. SCC Units: Thousand C		ns Transferred or Handled
4. Maximum Hourly 6,670	Rate: 5.	Maximum 58,409,928	Annual Rate:		Estimated Annual Activity Factor:
7. Maximum % Sulfu	ır: 8.	Maximum	% Ash:	9.	Million Btu per SCC Unit:
_	10. Segment Comment: The maximum hourly and annual rates shown in Fields 4 and 5 are the design water circulation rate.				
Segment Description	and Rate:	Segment	of		
1. Segment Description (Process/Fuel Type):					
2. Source Classificati	on Code (S	CC):	3. SCC Units:	•	
4. Maximum Hourly	Rate: 5.	Maximum	Annual Rate:	I	Estimated Annual Activity Factor:
7. Maximum % Sulft	ır: 8.	Maximum	% Ash:	9.	Million Btu per SCC Unit:
10. Segment Commen	t:			ı	

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### E. EMISSIONS UNIT POLLUTANTS

### List of Pollutants Emitted by Emissions Unit

1. Pollutant Emitted	Primary Control     Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
PM			WS
PM10			WS
_			
-			
		<del></del>	

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POLLUTANT DETAIL INFORMATION
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### F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted: PM	2. Total Perc	ent Efficie	ency of Control:
3.	Potential Emissions:		_	netically Limited?
	1.48 lb/hour 6.48	3 tons/year	Y	es x No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
	to tons/year			<u>-</u>
6.	Emission Factor:			7. Emissions
				Method Code:
	Reference: Vendor Data, mass balance			5
8.	Calculation of Emissions: Potential emissions are based on the design	cooling towers	vater flow	the design drift rate
	and the cycled water total dissolved solids.	cooming tower v	valci ilow	, the design drift rate
	Design water flow = 111,130 gpm = 55,609	452 lb/hr		
	Design drift rate = $0.0005\%$ of design water			
	Total dissolved solids = 5,331 ppm			
	Hourly PM emissions = $55,542,774$ lb/hr x			
	The maximum annual PM emissions = $1.48$	1b/hr x 8,760 h	r/yr x ton/	2,000  lb = 6.48  tpy
9.	Pollutant Potential/Estimated Fugitive Emis	sions Commen	t:	

Allowable Emissions __ of ___

## POLLUTANT DETAIL INFORMATION Page [2] of [4]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year
	Method of Compliance:		
6.	Allowable Emissions Comment (Description	of C	Operating Method):
Al	lowable Emissions Allowable Emissions	of _	
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:	•	
6.	Allowable Emissions Comment (Description	of (	Operating Method):
<u>Al</u>	lowable Emissions Allowable Emissions	of_	_
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:		
6.	Allowable Emissions Comment (Description	of (	Operating Method):

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### POLLUTANT DETAIL INFORMATION Page [3] of [4]

# F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

#### Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted: PM10	2. Total Perc	ent Efficie	ency of Control:
3.	Potential Emissions:		4. Synth	netically Limited?
	0.43 lb/hour 1.83	7 tons/year	□ Y	es x No
5.	Range of Estimated Fugitive Emissions (as to tons/year	applicable):		
6	Emission Factor:			7. Emissions
"	· ·	•		Method Code:
	Reference: Vendor Data			5
8.	Calculation of Emissions:  Potential emissions are based on the design the cycled water total dissolved solids, and to PM ₁₀ emissions occur when the cycled water total dissolved solids value the percent of Pl Design water flow = 111,130 gpm = 55,542 Design drift rate = 0.0005 percent of design Total dissolved solids = 3,918 ppm  Percent of PM that is PM ₁₀ = 39.14 percent Hourly PM ₁₀ emissions = 55,542,774 lb/hr = 0.426 lb/hr  The maximum annual PM ₁₀ emissions = 0.44	the percent of P or total dissolve M that is PM ₁₀ 1,774 lb/hr water flow x 0.0005% x 3,9	M that is led solids is equal to	PM ₁₀ . The maximum 3,918 ppm. At this 39.14 percent.
9.	Pollutant Potential/Estimated Fugitive Emis	sions Commen	t:	

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### POLLUTANT DETAIL INFORMATION Page [4] of [4]

# F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions	of
1. Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:
	lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description	
Allowable Emissions Allowable Emissions	
Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions: lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description	
Allowable Emissions Allowable Emissions	
Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3. Allowable Emissions and Units:	4. Equivalent Allowable Emissions:  lb/hour tons/year
5. Method of Compliance:	
6. Allowable Emissions Comment (Description	n of Operating Method):

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#### G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

<u>Visible Emissions Limitation:</u> Visible Emissi	ons Limitation of
1. Visible Emissions Subtype:	2. Basis for Allowable Opacity:  Rule Other
3. Allowable Opacity: Normal Conditions:	ceptional Conditions: % ed: min/hour
4. Method of Compliance:	
5. Visible Emissions Comment:	
Visible Emissions Limitation: Visible Emissi	ons Limitation of
1. Visible Emissions Subtype:	2. Basis for Allowable Opacity:
_	☐ Rule ☐ Other
3. Allowable Opacity: Normal Conditions: % Ex Maximum Period of Excess Opacity Allower	cceptional Conditions: %
Normal Conditions: % Ex	cceptional Conditions: %

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#### H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

<u>Continuous Monitoring System:</u> Continuous Monitor _ of _

1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	☐ Rule ☐ Other
4.	Monitor Information Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	
Co	ontinuous Monitoring System: Continuous	Monitor _ of _
1.	Parameter Code:	2. Pollutant(s):
3.	CMS Requirement:	Rule Other
4.	Monitor Information Manufacturer:	
	Model Number:	Serial Number:
5.	Installation Date:	6. Performance Specification Test Date:
7.	Continuous Monitor Comment:	

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### **EMISSIONS UNIT INFORMATION**

Section [6]

of [6]

#### I. EMISSIONS UNIT ADDITIONAL INFORMATION

### Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID: NA Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)    Attached, Document ID: Attach. M Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)  Attached, Document ID: Previously Submitted, Date  Not Applicable (construction application)
5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)    X Attached, Document ID: Attach. O   Previously Submitted, Date   Not Applicable
6.	Compliance Demonstration Reports/Records  Attached, Document ID:  Test Date(s)/Pollutant(s) Tested:
	Previously Submitted, Date:  Test Date(s)/Pollutant(s) Tested:
	To be Submitted, Date (if known):  Test Date(s)/Pollutant(s) Tested:
	× Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute  Attached, Document ID: × Not Applicable

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#### **EMISSIONS UNIT INFORMATION**

Section [6] of

### **Additional Requirements for Air Construction Permit Applications**

[6]

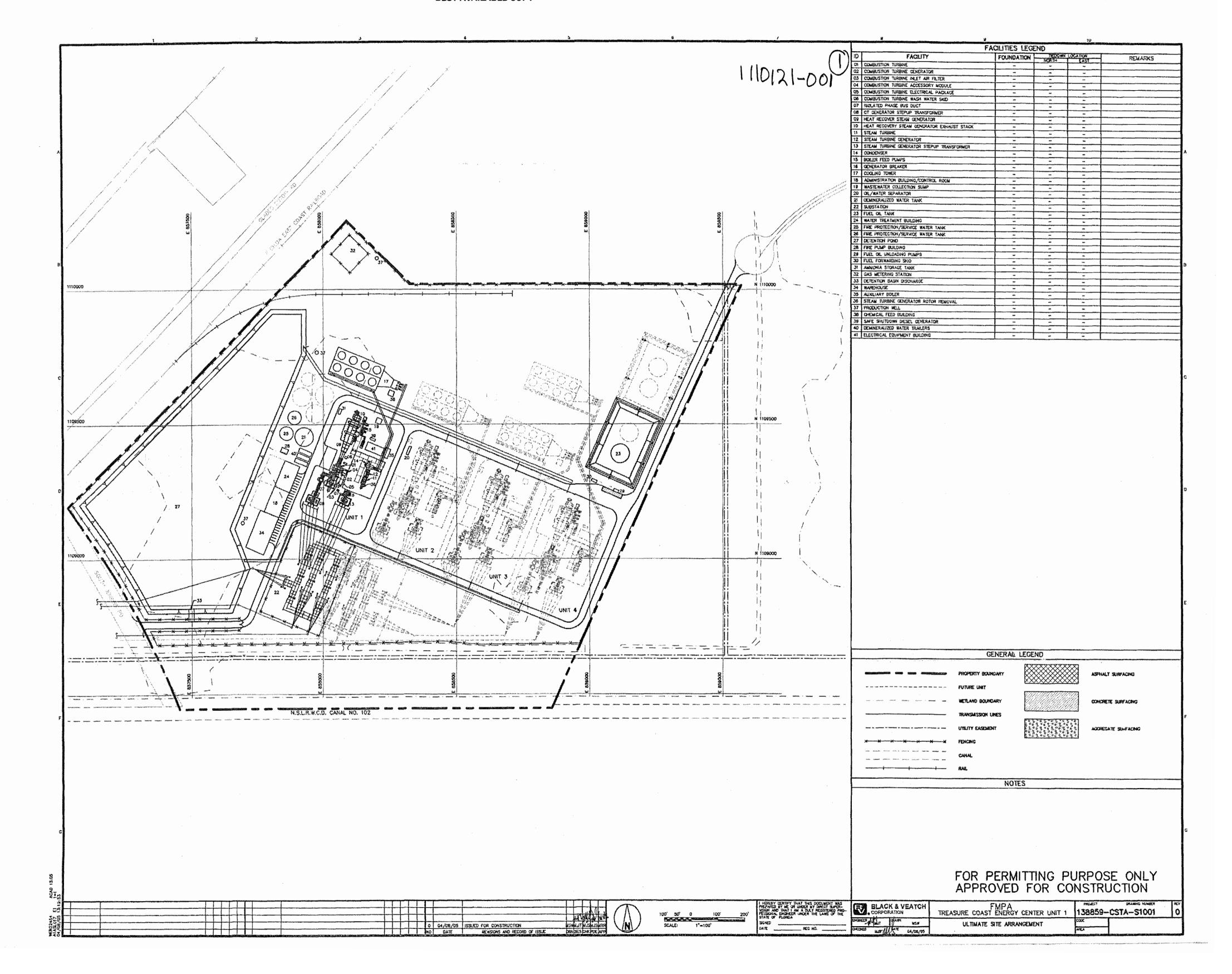
<u> </u>
1. Control Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7),
F.A.C.; 40 CFR 63.43(d) and (e))
x Attached, Document ID: Attach. P Not Applicable
2. Good Engineering Practice Stack Height Analysis (Rule 62-212.400(5)(h)6., F.A.C., and
Rule 62-212.500(4)(f), F.A.C.)
Attached, Document ID: Not Applicable
3. Description of Stack Sampling Facilities (Required for proposed new stack sampling facilities only)
Attached, Document ID: x Not Applicable
Tituenea, Document 1D
Additional Requirements for Title V Air Operation Permit Applications
1. Identification of Applicable Requirements
Attached, Document ID:
2. Compliance Assurance Monitoring
Attached, Document ID: Not Applicable
3. Alternative Methods of Operation
Attached, Document ID: Not Applicable
4. Alternative Modes of Operation (Emissions Trading)
Attached, Document ID: Not Applicable
5. Acid Rain Part Application
☐ Certificate of Representation (EPA Form No. 7610-1)
Copy Attached, Document ID:
☐ Acid Rain Part (Form No. 62-210.900(1)(a))
Attached, Document ID:
Previously Submitted, Date:
Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
Attached, Document ID:
Previously Submitted, Date:
☐ New Unit Exemption (Form No. 62-210.900(1)(a)2.)
Attached, Document ID:
Previously Submitted, Date:
Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)
Attached, Document ID:
Previously Submitted, Date:
Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)
Attached, Document ID:
Previously Submitted, Date:
Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)
Attached, Document ID:
Previously Submitted, Date:
Not Applicable

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Additional Requirements Comment	

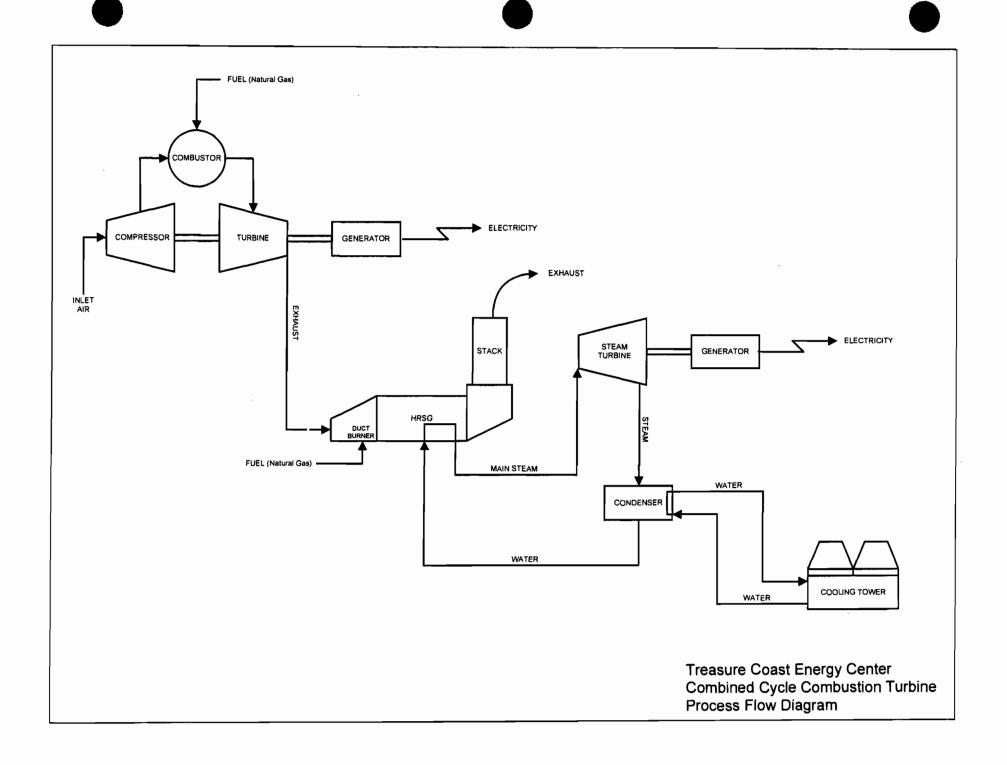
Attachment A

**Facility Plot Plan** 



Attachment B

**Process Flow Diagram** 



•	Attachment C  Precautions to Prevent Emissions of Unconfined Particulate Matter

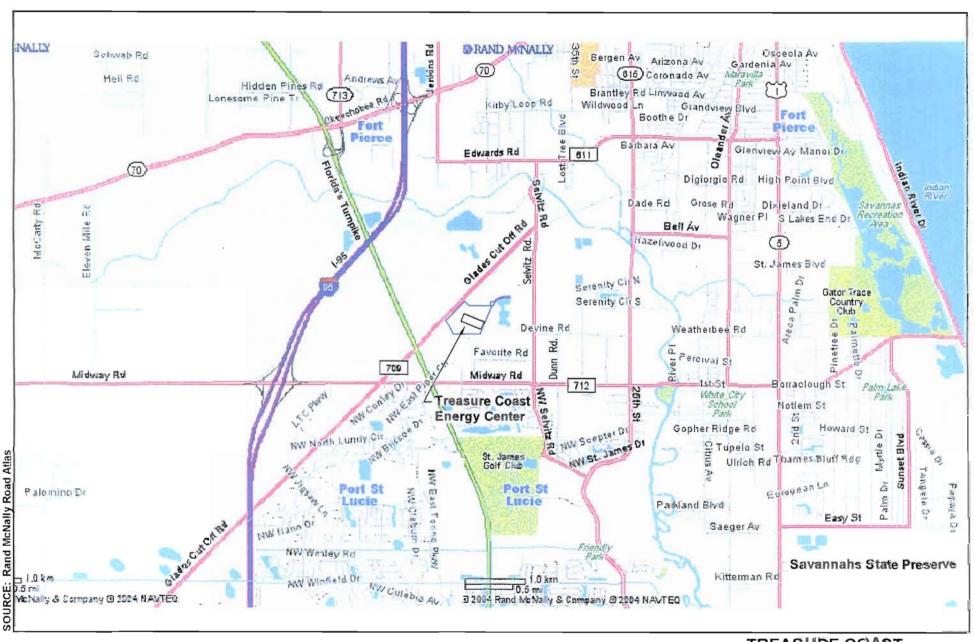
Attachment C - Precautions to Prevent Emissions of Unconfined Particulate Matter

### **Precautions to Prevent Emissions of Unconfined Particulate Matter**

Reasonable precautions to control unconfined emissions of particulate matter as listed in Rule 62-296.320(4), FAC will be employed as appropriate. Additionally, watering will be used as needed to prevent emissions from unpaved areas.

### Attachment D

**Area Map Showing Facility Location** 









TREASURE COAST ENERGY CENTER PROPOSED PROJECT LOCATION FIGURE 2-1

### Attachment E

**Description of Proposed Construction or Modification** 

#### **Description of Proposed Construction or Modification**

The Florida Municipal Power Agency (FMPA) proposes to install a 1x1 F-Class Combined Cycle Unit (Project) at the new Treasure Coast Energy Center, near Fort Pierce, St. Lucie County, Florida. The Project will include a 1x1 combined cycle unit (Unit 1) which will include a combustion turbine generator (CTG), heat recovery steam generator (HRSG), and a steam turbine generator (STG), operating at a nominal rating of 300 MW. New major support facilities include an approximately 990,000 gallon fuel oil storage tank, a natural gas fired auxiliary boiler, a diesel engine driven fire pump and associated 500 gallon fuel oil storage tank, a safe shutdown diesel generator and associated 1,000 gallon fuel oil storage tank, and a mechanical draft cooling tower. A more detailed description of the proposed construction can be found in the application technical support document accompanying this application.

Attachment F

Rule Applicability Analysis

#### Rule Applicability Analysis

### Rule Applicability Analysis for the Entire Facility

State: Rule 62-4.070 – Standards for Issuing or Denying Permits.

State: Rule 62-210.300 – Permits Required.

State: Rule 62-212.300 – General Preconstruction Review Requirements.

State: Rule 62-212.400 – Prevention of Significant Deterioration.

### Rule Applicability Analysis for the GE 7FA Combined Cycle Combustion Turbine

NOT APPLICABLE - Federal: 40 CFR Part 63 Subpart YYYY, National Emission Standards for Stationary Combustion Turbines. This standard is only applicable to emission units at a facility that is a major source of HAPs. Because the Treasure Coast Energy Center will not be a major source of HAPs, 40 CFR 63 Subpart YYYY does not apply to the combustion turbine.

May Become Applicable - Federal: 40 CFR Part 60 Subpart KKKK – Standards of Performance for Stationary Gas Turbines – Proposed Rule Published in the Federal Register on February 18, 2005. When/if this proposed rule becomes final as published it will apply to Unit 1.

The following rules are applicable to the Combined Cycle Combustion Turbine:

Federal: 40 CFR Part 60 Subpart GG (Rule 62-204.800(8)(b).39) – Standards of Performance for Stationary Gas Turbines. If/when proposed NSPS Subpart KKKK published in the Federal Register on February 18, 2005 becomes final as proposed, because Unit 1 would become subject to Subpart KKKK, it would not be subject to Subpart GG.

Federal: 40 CFR Part 60 Subpart Da (Rule 62-204.800(8)(b).39) – Standards of Performance for Electric Utility Steam Generators for Which Construction is Commenced After September 18, 1978. If/when proposed NSPS Subpart KKKK published in the Federal Register on February 18, 2005 and proposed revisions to Subpart Da published in the Federal Register on February 28, 2005 become final as proposed, because the duct burner would be covered under Subpart KKKK, it would not be subject to Subpart Da.

Federal: 40 CFR Part 60 Subpart A – General Provisions.

Federal: 40 CFR Part 72 – Permits Regulation (Acid Rain)

Federal: 40 CFR Part 75 - Continuous Emissions Monitoring

State: Rule 62-204.800(8)(d) – General Provisions Adopted – 40 CFR 60 Subpart A – General Provisions adopted by reference, with exceptions.

Attachment F – Rule Applicability Analysis

State: Rule 62-212.400 – Prevention of Significant Deterioration applies to CO, NO_x, SO₂, PM, PM₁₀, and sulfuric acid mist. See the technical support document accompanying this application for a more detailed discussion of PSD applicability.

State: Rule 62-212.300 – General Preconstruction Review Requirements. Applies to applicable pollutants not subject to PSD review.

State: Rule 62-297.310 – General Compliance Test Requirements.

### Rule Applicability Analysis for the Natural Gas Auxiliary Boiler

NOT APPLICABLE - Federal: 40 CFR Part 60 Subpart Dc, Standards of Performance for Small Industrial-Commercial-Institutional Steam Generating Units. This standard applies to each steam generating unit that has a maximum design capacity of 100 mmBtu/hr or less, but greater than 10 mmBtu/hr. Because the Project natural gas auxiliary boiler has a maximum heat input rate of less than 10 mmBtu/hr, it is not subject to 40 CFR 60 Subpart Dc.

The following rules are applicable to the Natural Gas Auxiliary Boiler:

State: Rule 62-212.400 – Prevention of Significant Deterioration (PSD)

State: Rule 62-296.406, F.A.C., Fossil Fuel Steam Generators with Less Than 250 Million Btu Per Hour Heat Input, New and Existing Units.

State: Rule 62-297.310 – General Compliance Test Requirements.

#### Rule Applicability Analysis for the Diesel Engine Fire Pump

NOT APPLICABLE - Federal: 40 CFR Part 63 Subpart ZZZZ, National Emission Standards for Recipricating Internal Combustion Engines. This standard is only applicable to emission units at a facility that is a major source of HAPs. Because the Treasure Coast Energy Center will not be a major source of HAPs, 40 CFR 63 Subpart ZZZZ does not apply to the diesel engine fire pump.

The following rules are applicable to the Diesel Engine Fire Pump: State: Rule 62-212.400 – Prevention of Significant Deterioration (PSD)

#### Rule Applicability Analysis for the Safe Shutdown Diesel Generator

NOT APPLICABLE - Federal: 40 CFR Part 63 Subpart ZZZZ, National Emission Standards for Recipricating Internal Combustion Engines. This standard is only applicable to emission units at a facility that is a major source of HAPs. Because the Treasure Coast Energy Center will not be a major source of HAPs, 40 CFR 63 Subpart ZZZZ does not apply to the safe shutdown diesel generator.

The following rules are applicable to the Safe Shutdown Diesel Generator: State: Rule 62-212.400 – Prevention of Significant Deterioration (PSD)

### Rule Applicability Analysis for the 990,000 Gallon No. 2 Fuel Oil Storage Tank

NOT APPLICABLE - Federal: 40 CFR Part 60 Subpart Kb, AS REVISED OCTOBER 15, 2003 – Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984. Because the vapor pressure of No. 2 fuel oil is less than 3.5 kPa, this storage tank is not subject to 40 CFR Part 60 Subpart Kb.

NOT APPLICABLE - State: Rule 62-212.300 – General Preconstruction Review Requirements. Per 62-210(3), F.A.C., this emissions unit is exempt from the permitting requirements of Chapter 62-212, F.A.C. because it satisfies the applicable criteria of paragraph 62-210.300(3)(b)1., F.A.C.

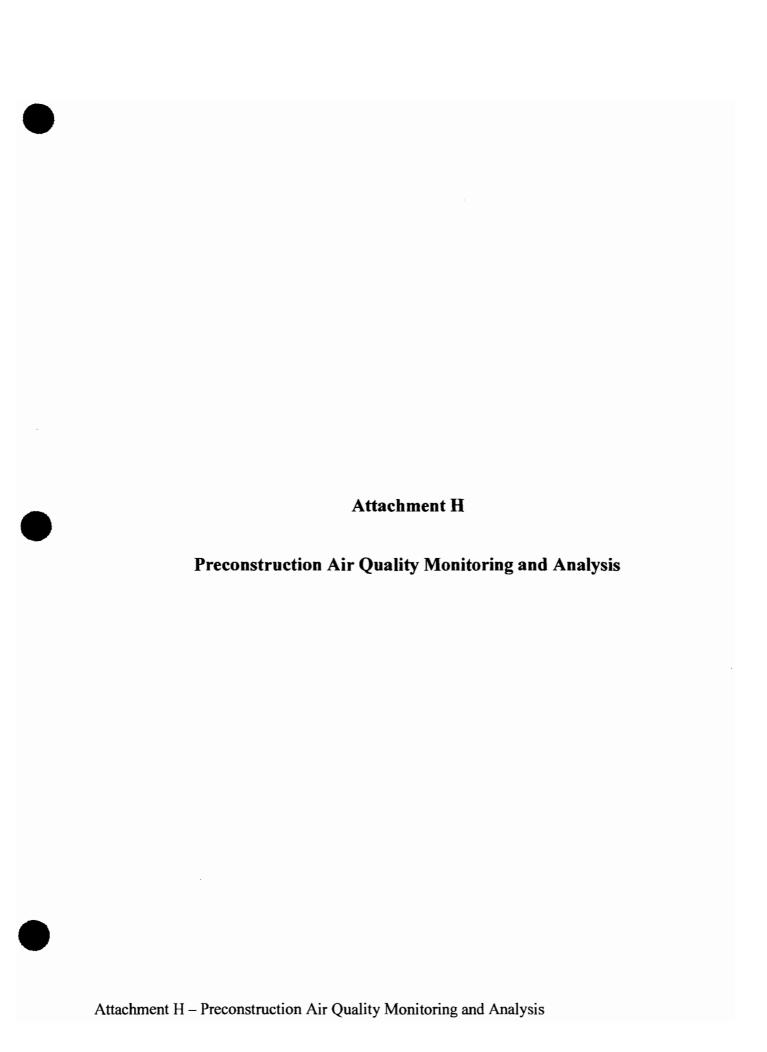
Attachment G

List of Exempt Emission Units

### **List of Exempt Emission Units**

The 990,000 gallon fuel oil storage tank is exempt from the requirement to obtain an air construction permit. The unit is exempt in accordance with Rule 62-210.300(3)(b)1., F.A.C.

The Diesel Engine Fire Pump is exempt from the requirement to obtain an air construction permit. The unit is exempt in accordance with Rule 62-210.300(3)(a)22., F.A.C.



## Preconstruction Air Quality Monitoring and Analysis

Preconstruction air quality monitoring is addressed in Section 4.0 of the technical support document included with this application.

Attachment I

**Ambient Impact Analysis** 

# **Ambient Impact Analysis**

The ambient impact analysis is included as Section 4.0 of the technical support document included with this application.

## Attachment J

**Air Quality Impact Since 1977** 

# **Air Quality Impact Since 1977**

A discussion of the Air Quality Impact since 1977 is included in Section 5 of the technical support document included with this application.

Attachment K

**Additional Impact Analyses** 

# **Additional Impact Analyses**

Additional Impact Analyses are included in Section 5 of the technical support document included with this application.

## Attachment L

Fuel Analysis or Specification

# Fuel Analysis or Specification

Fuel is specified as pipeline natural gas or No. 2 fuel oil containing no more than 0.0015 percent sulfur.	

### Attachment M

**Detailed Description of Control Equipment** 

### **Detailed Description of Control Equipment**

Dry Low-NO_x Burners: Dry low-NO_x burners are used to reduce flame temperature as a means to control NO_x emissions. A more detailed discussion of dry low-NO_x burners is included in Attachment 4 of the application support document.

Water Injection: A control technology used to limit  $NO_x$  emissions. The thermal  $NO_x$  contribution to total  $NO_x$  emissions is reduced by lowering the combustion temperature through the use of water injection in the combustion zones of the combustion turbine. A more detailed discussion of water injection is included in Attachment 4 of the application support document.

Selective Catalytic Reduction (SCR): A post-combustion control technology used to limit NO_x emissions. The SCR process combines vaporized ammonia with NO_x in the presence of a catalyst to form nitrogen and water. A more detailed discussion of the SCR control system is included in Attachment 4 of the application support document.

Drift Eliminators: The mechanical draft cooling tower will include drift eliminator to achieve a design drift rate of 0.0005 percent, thus minimizing PM and PM₁₀ emissions.

## Attachment N

Procedures for Startup and Shutdown

# Procedures for Startup and Shutdown

Procedures for startup and shutdown will be completed in accordance with manufacturers' operating procedures and/or plant operating procedures.

Attachment O

Operation and Maintenance Plan

## **Operation and Maintenance Plan**

The emission units will be operated and maintained in accordance with manufacturer's recommendations, operations and maintenance experience, and technical guidance taking into account protection of equipment, safety of personnel and other factors as deemed necessary to maintain compliance with the permitted limits.

## Attachment P

Control Technology Review and Analysis

# Control Technology Review and Analysis

The control technology review and analysis is included as Attachment 4 of the application support document included with this application.

# Attachment Q

**Good Engineering Practice Stack Height Analysis** 

# **Good Engineering Practice Stack Height Analysis**

A good engineering practice stack height analysis is included in Section 4.2.3 of the application support document included with this application.

# Attachment R

**Description of Stack Sampling Facilities** 

### **Description of Stack Sampling Facilities**

Unit 1 will be equipped with stack sampling facilities appropriate for performing required stack testing. A detailed description of stack sampling facilities is not available at this time. When available, if requested by the Department, the stack sampling facilities description will be supplied to the Department.

# Attachment S

Air Dispersion Modeling Files (CD)

