



**DECKER ENERGY  
INTERNATIONAL**

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**JUN 12 2000**

**BUREAU OF AIR REGULATION**

June 7, 2000

Administrator, New Source Review Section  
Florida Department of Environmental Protection  
2600 Blair Stone Road  
Tallahassee, Florida 32399-2400

Attention: Mr. A.A. Linero, P.E.

*1050336-001-AC  
PSD-FI-292*

RE: PEACE RIVER STATION, L.L.C.  
AIR PERMIT APPLICATION AND PREVENTION OF SIGNIFICANT  
DETERIORATION ANALYSIS  
PEACE RIVER STATION POWER PROJECT, POLK COUNTY, FLORIDA

Dear Mr. Linero:

Peace River Station, L.L.C. is pleased to submit this application for a permit to license, construct, and operate an independent power production facility in Polk County, Florida. The application includes supportive information that the project is required to provide under the regulations for Prevention of Significant Deterioration (PSD) of air quality. The application processing fee of \$7,500 is included with this transmittal.

We appreciate your timely review of this application and look forward towards working with you. If you have any questions, please contact me or Mr. Jon Pomerleau at (407) 628-8900.

Sincerely,

PEACE RIVER STATION, L.L.C.

*Jon T. Pomerleau, Jr.  
For Macauley Whiting, Jr.*

Macauley Whiting, Jr.  
President

Cc: Jon T. Pomerleau  
K.F.Kosky- Golder Associates  
R.C.McCann- Golder Associates

*cc: J. Koerner, BAR  
SWD  
polk CO  
EPA  
NPS  
C. Carlson*

DA

Peace River Station, LLC

7243

DECKER ENERGY INTERNATIONAL, INC.

P O BOX 2397 PH 407-628-8800  
WINTER PARK, FL 32790

62-751/931  
BRANCH 0094

DATE June 8, 2000

PAY TO THE ORDER OF Florida Dept. of Environmental Protection \$ 7500.00

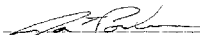
Seven Thousand Five Hundred Exactly\*\*\*\*\* DOLLARS

**FIRST UNION**

First Union National Bank

RT 662107513

FOR Air Permit/Peace River Sta.



**RECEIVED**

**JUN 12 2000**

**BUREAU OF AIR REGULATION**

**AIR PERMIT APPLICATION AND PREVENTION  
OF SIGNIFICANT DETERIORATION ANALYSIS  
FOR THE PEACE RIVER STATION,  
POLK COUNTY, FLORIDA**

**Prepared For:**

**Peace River Station, L.L.C.  
163 East Morse Boulevard, Suite 200  
Winter Park, Florida 32790**

**Prepared By:**

**Golder Associates Inc.  
6241 NW 23rd Street, Suite 500  
Gainesville, Florida 32653-1500**

**June 2000  
9939562Y/F1**

**DISTRIBUTION:**

**7 Copies - Florida Department of Protection  
2 Copies - Peace River Station, L.L.C.  
2 Copies - Golder Associates Inc.**

## TABLE OF CONTENTS

PART A -- AIR PERMIT APPLICATION

PART B -- REPORT

<u>SECTION</u>	<u>PAGE</u>
1.0 INTRODUCTION .....	1-1
2.0 PROJECT DESCRIPTION .....	2-1
2.1 SITE DESCRIPTION .....	2-1
2.2 POWER PLANT .....	2-1
2.3 PROPOSED SOURCE EMISSIONS AND STACK PARAMETERS .....	2-2
2.4 SITE LAYOUT, STRUCTURES, AND STACK SAMPLING FACILITIES.....	2-4
3.0 AIR QUALITY REVIEW REQUIREMENTS AND APPLICABILITY .....	3-1
3.1 NATIONAL AND STATE AAQS .....	3-1
3.2 PSD REQUIREMENTS .....	3-1
3.2.1 GENERAL REQUIREMENTS.....	3-1
3.2.2 CONTROL TECHNOLOGY REVIEW.....	3-3
3.2.3 SOURCE IMPACT ANALYSIS .....	3-5
3.2.4 AIR QUALITY MONITORING REQUIREMENTS .....	3-8
3.2.5 SOURCE INFORMATION/GOOD ENGINEERING PRACTICE STACK HEIGHT .....	3-8
3.2.6 ADDITIONAL IMPACT ANALYSIS.....	3-9
3.3 NONATTAINMENT RULES .....	3-10
3.4 EMISSION STANDARDS .....	3-10
3.4.1 NEW SOURCE PERFORMANCE STANDARDS .....	3-10
3.4.2 FLORIDA RULES .....	3-12
3.4.3 FLORIDA AIR PERMITTING REQUIREMENTS .....	3-13
3.4.4 HAZARDOUS POLLUTANT REVIEW .....	3-13
3.4.5 LOCAL AIR REGULATIONS .....	3-13
3.5 SOURCE APPLICABILITY.....	3-14

## TABLE OF CONTENTS

3.5.1	AREA CLASSIFICATION.....	3-14
3.5.2	PSD REVIEW .....	3-14
3.5.3	NONATTAINMENT REVIEW .....	3-16
3.5.4	OTHER CLEAN AIR ACT REQUIREMENTS .....	3-16
4.0	CONTROL TECHNOLOGY REVIEW.....	4-1
4.1	APPLICABILITY .....	4-1
4.2	NEW SOURCE PERFORMANCE STANDARDS .....	4-1
4.3	BEST AVAILABLE CONTROL TECHNOLOGY.....	4-2
4.3.1	PROPOSED BACT .....	4-2
4.3.2	NITROGEN OXIDES.....	4-2
4.3.3	CARBON MONOXIDE.....	4-11
4.3.4	SO <sub>2</sub> AND H <sub>2</sub> SO <sub>4</sub> POLLUTANT EMISSIONS .....	4-13
4.3.5	PM/PM <sub>10</sub> , SO <sub>2</sub> AND OTHER REGULATED AND NONREGULATED POLLUTANT EMISSIONS .....	4-13
5.0	AMBIENT MONITORING ANALYSIS.....	5-1
6.0	AIR QUALITY IMPACT ANALYSIS.....	6-1
6.1	SIGNIFICANT IMPACT ANALYSIS APPROACH .....	6-1
6.2	PRECONSTRUCTION MONITORING ANALYSIS APPROACH .....	6-1
6.3	AIR MODELING ANALYSIS APPROACH .....	6-2
6.3.1	GENERAL PROCEDURES .....	6-2
6.3.2	MODEL SELECTION .....	6-3
6.3.3	METEOROLOGICAL DATA.....	6-5
6.3.4	EMISSION INVENTORY .....	6-6
6.3.5	RECEPTOR LOCATIONS.....	6-6
6.3.6	BUILDING DOWNWASH EFFECTS.....	6-8
6.4	SIGNIFICANT IMPACT ANALYSIS RESULTS .....	6-9
6.4.1	SITE VICINITY .....	6-9
6.4.2	PSD CLASS I AREA.....	6-9

**TABLE OF CONTENTS**

7.0 ADDITIONAL IMPACT ANALYSIS..... 7-1

7.1 IMPACTS DUE TO DIRECT GROWTH ..... 7-1

7.2 IMPACT ON SOILS, VEGETATION, WILDLIFE, AND VISIBILITY IN THE  
PROJECT'S VICINITY ..... 7-1

7.3 IMPACTS UPON PSD CLASS I AREAS..... 7-3

7.3.1 IDENTIFICATION OF AQRVS AND METHODOLOGY..... 7-3

7.3.2 IMPACTS TO SOILS..... 7-5

7.3.3 IMPACTS TO VEGETATION..... 7-6

7.3.4 IMPACTS TO WILDLIFE..... 7-13

7.3.5 IMPACTS UPON VISIBILITY..... 7-14

8.0 REFERENCES ..... 8-1

## TABLE OF CONTENTS

### LIST OF TABLES

2-1	Stack, Operating, and Emission Data for Simple Cycle Combustion Turbine, Natural Gas Firing.....	2-5
2-2	Stack, Operating, and Emission Data for the Simple Cycle Combustion Turbine, Distillate Fuel Oil Firing.....	2-6
2-3	Summary of Maximum Potential Annual Emissions for the Simple Cycle Combustion Turbine Project.....	2-7
2-4	Maximum Potential Annual Emissions for the Simple Cycle Combustion Turbine Project Compared to the PSD Significant Emission Rates.....	2-8
3-1	National and State AAQS, Allowable PSD Increments, and Significant Impact Levels.....	3-18
3-2	PSD Significant Emission Rates and <i>De Minimis</i> Monitoring Concentrations.....	3-19
3-3	Maximum Emissions Due to the Proposed Peace River Station Compared to the PSD Significant Emission Rates.....	3-20
3-4	Predicted Net Increase in Impacts Due to the Proposed Peace River Station Compared to PSD <i>De Minimis</i> Monitoring Concentrations.....	3-21
4-1	NO <sub>x</sub> Emission Estimates (TPY) of BACT Alternative Technologies (per Unit).....	4-15
6-1	Major Features of the ISCST3 Model.....	6-11
6-2	Maximum Pollutant Concentrations Predicted for Three Simple-Cycle Combustion Turbines Firing Natural Gas and Distillate Fuel Oil by Operating Load and Inlet Ambient Temperature.....	6-12
6-3	Summary of Maximum Pollutant Concentrations Predicted for Three Simple-Cycle Combustion Turbines Compared to the EPA Class II Significant Impact Levels, PSD Class II Increments, and AAQS.....	6-13
6-4	Maximum Pollutant Concentrations Predicted for Three Simple-Cycle Combustion Turbines Firing Natural Gas and Distillate Fuel Oil by Operating Load and Inlet Ambient Temperature at the PSD Class I Area of the Chassahowitzka NWA.....	6-14
6-5	Summary of Maximum Pollutant Concentrations Predicted for Three Simple-Cycle Combustion Turbines Compared to the EPA Class I Significant Impact Levels and PSD Class I Increments.....	6-15
7-1	Maximum Pollutant Concentrations Due to Peace River Station Predicted at the PSD Class I Area of the Chassahowitzka National Wilderness Area.....	7-17
7-2	SO <sub>2</sub> Effects Levels for Various Plant Species.....	7-18

## TABLE OF CONTENTS

### LIST OF TABLES - Continued

7-3	Sensitivity Groupings of Vegetation Based on Visible Injury at Different SO <sub>2</sub> Exposures .....	7-19
7-4	Examples of Reported Effects of Air Pollutants at Concentrations Below National Secondary Ambient Air Quality Standards.....	7-20
7-5	Maximum Pollutant Concentrations Predicted for the Peace River Station at the Chassahowitzka PSD Class I Area.....	7-21
7-6	Computed Daily Average RH Factors for Days of Maximum Impacts Predicted for the Peace River Station at the PSD Class I area of the Chassahowitzka NWA.....	7-22
7-7	Summary of the Refined Regional Haze Analysis for the Peace River Station's Impacts Predicted at the PSD Class I Area of the Chassahowitzka NWA.....	7-23

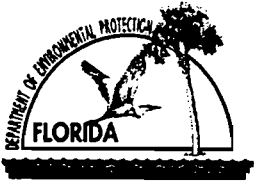
### LIST OF FIGURES

1-1	General Site Location.....	1-3
2-1	Site Location and Topographic Map .....	2-9
2-2	Simplified Flow Diagram of Proposed "F" Class .....	2-10
2-3	Simplified Flow Diagram of Proposed "F" Class .....	2-11
2-4	Simplified Flow Diagram of Proposed "F" Class .....	2-12
2-5	Plant Layout Overlay On Survey .....	2-13



**PART A**

**AIR PERMIT APPLICATION**



# Department of Environmental Protection

## Division of Air Resources Management

### APPLICATION FOR AIR PERMIT - TITLE V SOURCE

See Instructions for Form No. 62-210.900(1)

#### I. APPLICATION INFORMATION

##### Identification of Facility

1. Facility Owner/Company Name: <b>Peace River Station, L.L.C.</b>	
2. Site Name: <b>Peace River Station</b>	
3. Facility Identification Number: <span style="float: right;"><input checked="" type="checkbox"/> Unknown</span>	
4. Facility Location: <b>¼ mile west of Fort Meade</b> Street Address or Other Locator: <b>West County Road 630</b> City: <b>Fort Meade</b> County: <b>Polk</b> Zip Code:	
5. Relocatable Facility? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	6. Existing Permitted Facility? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No

##### Application Contact

1. Name and Title of Application Contact: <b>Macauley Whiting, Jr., President</b>	
2. Application Contact Mailing Address: Organization/Firm: <b>Peace River Station, L.L.C.</b> Street Address: <b>163 East Morse Boulevard, Suite 200</b> City: <b>Winter Park</b> State: <b>FL</b> Zip Code: <b>32789</b>	
3. Application Contact Telephone Numbers: Telephone: <b>(407) 628 - 8900</b> Fax: <b>(407) 628 - 8535</b>	

##### Application Processing Information (DEP Use)

1. Date of Receipt of Application:	<i>June 12, 2000</i>
2. Permit Number:	<i>1050336-001-AC</i>
3. PSD Number (if applicable):	<i>PSD-FI-292</i>
4. Siting Number (if applicable):	

**Purpose of Application**

**Air Operation Permit Application**

This Application for Air Permit is submitted to obtain: (Check one)

[ ] Initial Title V air operation permit for an existing facility which is classified as a Title V source.

[ ] Initial Title V air operation permit for a facility which, upon start up of one or more newly constructed or modified emissions units addressed in this application, would become classified as a Title V source.

Current construction permit number: \_\_\_\_\_

[ ] Title V air operation permit revision to address one or more newly constructed or modified emissions units addressed in this application.

Current construction permit number: \_\_\_\_\_

Operation permit number to be revised: \_\_\_\_\_

[ ] Title V air operation permit revision or administrative correction to address one or more proposed new or modified emissions units and to be processed concurrently with the air construction permit application. (Also check Air Construction Permit Application below.)

Operation permit number to be revised/corrected: \_\_\_\_\_

[ ] Title V air operation permit revision for reasons other than construction or modification of an emissions unit. Give reason for the revision; e.g., to comply with a new applicable requirement or to request approval of an "Early Reductions" proposal.

Operation permit number to be revised: \_\_\_\_\_

Reason for revision: \_\_\_\_\_

**Air Construction Permit Application**

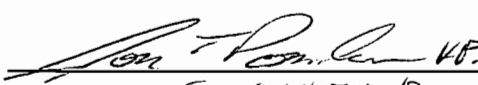
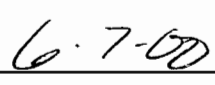
This Application for Air Permit is submitted to obtain: (Check one)

[ X ] Air construction permit to construct or modify one or more emissions units.

[ ] Air construction permit to make federally enforceable an assumed restriction on the potential emissions of one or more existing, permitted emissions units.

[ ] Air construction permit for one or more existing, but unpermitted, emissions units.

**Owner/Authorized Representative or Responsible Official**

1. Name and Title of Owner/Authorized Representative or Responsible Official: <b>Macauley Whiting, Jr., President</b>
2. Owner/Authorized Representative or Responsible Official Mailing Address: Organization/Firm: <b>Peace River Station, L.L.C.</b> Street Address: <b>163 East Morse Boulevard, Suite 200</b> City: <b>Winter Park</b> State: <b>FL</b> Zip Code: <b>32789</b>
3. Owner/Authorized Representative or Responsible Official Telephone Numbers: Telephone: <b>( 407 ) 628 - 8900</b> Fax: <b>( 407 ) 628 - 8535</b>
4. Owner/Authorized Representative or Responsible Official Statement: <i>I, the undersigned, am the owner or authorized representative*(check here [ ], if so) or the responsible official (check here [ ], if so) of the Title V source addressed in this application, whichever is applicable. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements made in this application are true, accurate and complete and that, to the best of my knowledge, any estimates of emissions reported in this application are based upon reasonable techniques for calculating emissions. The air pollutant emissions units and air pollution control equipment described in this application will be operated and maintained so as to comply with all applicable standards for control of air pollutant emissions found in the statutes of the State of Florida and rules of the Department of Environmental Protection and revisions thereof. I understand that a permit, if granted by the Department, cannot be transferred without authorization from the Department, and I will promptly notify the Department upon sale or legal transfer of any permitted emissions unit.</i>   Signature <i>FOR M. WHITING, JR.</i>  Date

\* Attach letter of authorization if not currently on file.

**Professional Engineer Certification**

1. Professional Engineer Name: <b>Kennard F. Kosky</b> Registration Number: <b>14996</b>
2. Professional Engineer Mailing Address: Organization/Firm: <b>Golder Associates Inc.</b> Street Address: <b>6241 NW 23rd Street, Suite 500</b> City: <b>Gainesville</b> State: <b>FL</b> Zip Code: <b>32653-1500</b>
3. Professional Engineer Telephone Numbers: Telephone: <b>( 352 ) 336 - 5600</b> Fax: <b>( 352 ) 336 - 6603</b>

4. Professional Engineer Statement:

*I, the undersigned, hereby certify, except as particularly noted herein\*, that:*

*(1) To the best of my knowledge, there is reasonable assurance that the air pollutant emissions unit(s) and the air pollution control equipment described in this Application for Air Permit, when properly operated and maintained, will comply with all applicable standards for control of air pollutant emissions found in the Florida Statutes and rules of the Department of Environmental Protection; and*

*(2) To the best of my knowledge, any emission estimates reported or relied on in this application are true, accurate, and complete and are either based upon reasonable techniques available for calculating emissions or, for emission estimates of hazardous air pollutants not regulated for an emissions unit addressed in this application, based solely upon the materials, information and calculations submitted with this application.*

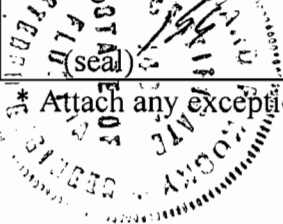
*If the purpose of this application is to obtain a Title V source air operation permit (check here [  ], if so), I further certify that each emissions unit described in this Application for Air Permit, when properly operated and maintained, will comply with the applicable requirements identified in this application to which the unit is subject, except those emissions units for which a compliance schedule is submitted with this application.*

*If the purpose of this application is to obtain an air construction permit for one or more proposed new or modified emissions units (check here [], if so), I further certify that the engineering features of each such emissions unit described in this application have been designed or examined by me or individuals under my direct supervision and found to be in conformity with sound engineering principles applicable to the control of emissions of the air pollutants characterized in this application.*

*If the purpose of this application is to obtain an initial air operation permit or operation permit revision for one or more newly constructed or modified emissions units (check here [  ], if so), I further certify that, with the exception of any changes detailed as part of this application, each such emissions unit has been constructed or modified in substantial accordance with the information given in the corresponding application for air construction permit and with all provisions contained in such permit.*

*Kamal F. Herby*  
\_\_\_\_\_  
Signature

*5/31/2000*  
\_\_\_\_\_  
Date



Attach any exception to certification statement.



**Construction/Modification Information**

1. Description of Proposed Project or Alterations:

**Construction of 3 170-MW GE Frame 7FA combustion turbines. See Attachment PSD-PRS.**

2. Projected or Actual Date of Commencement of Construction: **1 Dec 2000**

3. Projected Date of Completion of Construction: **1 Jun 2002**

**Application Comment**

**See Attachment PSD-PRS**

## II. FACILITY INFORMATION

### A. GENERAL FACILITY INFORMATION

#### Facility Location and Type

1. Facility UTM Coordinates: Zone: <b>17</b> East (km): <b>419.5</b> North (km): <b>3,069.7</b>			
2. Facility Latitude/Longitude: Latitude (DD/MM/SS): <b>27 / 45 / 4</b> Longitude (DD/MM/SS): <b>89 / 49 / 00</b>			
3. Governmental Facility Code: <b>0</b>	4. Facility Status Code: <b>C</b>	5. Facility Major Group SIC Code: <b>49</b>	6. Facility SIC(s): <b>4911</b>
7. Facility Comment (limit to 500 characters):  <b>Project consists of three 174-MW dual-fuel, General Electric Frame 7FA combustion turbines that will use dry low-nitrogen oxide combustion technology when firing natural gas and water injection when firing distillate fuel oil. Each CT will operate up to 3,390 hours per year.</b>			

#### Facility Contact

1. Name and Title of Facility Contact: <b>Macauley Whiting, Jr., President</b>			
2. Facility Contact Mailing Address: Organization/Firm: <b>Peace River Station, L.L.C.</b> Street Address: <b>163 East Morse Boulevard, Suite 200</b> City: <b>Winter Park</b> State: <b>FL</b> Zip Code: <b>32789</b>			
3. Facility Contact Telephone Numbers: Telephone: <b>( 407 ) 628 - 8900</b> Fax: <b>( 407 ) 628 - 8535</b>			



**Facility Regulatory Classifications**

**Check all that apply:**

1. <input type="checkbox"/> Small Business Stationary Source?	<input type="checkbox"/> Unknown
2. <input checked="" type="checkbox"/> Major Source of Pollutants Other than Hazardous Air Pollutants (HAPs)?	
3. <input type="checkbox"/> Synthetic Minor Source of Pollutants Other than HAPs?	
4. <input type="checkbox"/> Major Source of Hazardous Air Pollutants (HAPs)?	
5. <input type="checkbox"/> Synthetic Minor Source of HAPs?	
6. <input checked="" type="checkbox"/> One or More Emissions Units Subject to NSPS?	
7. <input type="checkbox"/> One or More Emission Units Subject to NESHAP?	
8. <input checked="" type="checkbox"/> Title V Source by EPA Designation?	
9. Facility Regulatory Classifications Comment (limit to 200 characters):	
<p><b>CTs are subject to NSPS Subpart GG. The oil storage tanks are subject to Subpart Kb.</b></p>	

**List of Applicable Regulations**

<b>Not Applicable</b>	

## B. FACILITY POLLUTANTS

### List of Pollutants Emitted

1. Pollutant Emitted	2. Pollutant Classif.	3. Requested Emissions Cap		4. Basis for Emissions Cap	5. Pollutant Comment
		lb/hour	tons/year		
PM	B				Particulate Matter-Total
VOC	B				Volatile Organic Compounds
SO <sub>2</sub>	A				Sulfur Dioxide
NO <sub>x</sub>	A				Nitrogen Oxides
CO	A				Carbon Monoxides
PM <sub>10</sub>	B				Particulate Matter-PM <sub>10</sub>



**Additional Supplemental Requirements for Title V Air Operation Permit Applications**

8. List of Proposed Insignificant Activities: <input type="checkbox"/> Attached, Document ID: _____ <input type="checkbox"/> Not Applicable
9. List of Equipment/Activities Regulated under Title VI: <input type="checkbox"/> Attached, Document ID: _____ <input type="checkbox"/> Equipment/Activities On site but Not Required to be Individually Listed <input type="checkbox"/> Not Applicable
10. Alternative Methods of Operation: <input type="checkbox"/> Attached, Document ID: _____ <input type="checkbox"/> Not Applicable
11. Alternative Modes of Operation (Emissions Trading): <input type="checkbox"/> Attached, Document ID: _____ <input type="checkbox"/> Not Applicable
12. Identification of Additional Applicable Requirements: <input type="checkbox"/> Attached, Document ID: _____ <input type="checkbox"/> Not Applicable
13. Risk Management Plan Verification: <input type="checkbox"/> Plan previously submitted to Chemical Emergency Preparedness and Prevention Office (CEPPO). Verification of submittal attached (Document ID: _____) or previously submitted to DEP (Date and DEP Office: _____) <input type="checkbox"/> Plan to be submitted to CEPPO (Date required: _____) <input type="checkbox"/> Not Applicable
14. Compliance Report and Plan: <input type="checkbox"/> Attached, Document ID: _____ <input type="checkbox"/> Not Applicable
15. Compliance Certification (Hard-copy Required): <input type="checkbox"/> Attached, Document ID: _____ <input type="checkbox"/> Not Applicable

**III. EMISSIONS UNIT INFORMATION**

A separate Emissions Unit Information Section (including subsections A through J as required) must be completed for each emissions unit addressed in this Application for Air Permit. If submitting the application form in hard copy, indicate, in the space provided at the top of each page, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application.

**A. GENERAL EMISSIONS UNIT INFORMATION  
(All Emissions Units)**

**Emissions Unit Description and Status**

<p>1. Type of Emissions Unit Addressed in This Section: (Check one)</p> <p><input checked="" type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).</p> <p><input type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.</p> <p><input type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only.</p>			
<p>2. Regulated or Unregulated Emissions Unit? (Check one)</p> <p><input checked="" type="checkbox"/> The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.</p> <p><input type="checkbox"/> The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.</p>			
<p>3. Description of Emissions Unit Addressed in This Section (limit to 60 characters): <b>GE Frame 7FA Combustion Turbine</b></p>			
<p>4. Emissions Unit Identification Number: ID:</p>		<p><input type="checkbox"/> No ID <input checked="" type="checkbox"/> ID Unknown</p>	
<p>5. Emissions Unit Status Code: <b>C</b></p>	<p>6. Initial Startup Date:</p>	<p>7. Emissions Unit Major Group SIC Code: <b>49</b></p>	<p>8. Acid Rain Unit? <input checked="" type="checkbox"/></p>
<p>9. Emissions Unit Comment: (Limit to 500 Characters)</p> <p><b>This emission unit is a GE Frame 7FA combustion turbine operating in simple cycle mode. See Attachment PSD-PRS.</b></p>			

**Emissions Unit Control Equipment**

1. Control Equipment/Method Description (Limit to 200 characters per device or method):

**Dry Low NO<sub>x</sub> combustion - Natural gas firing**

2. Control Device or Method Code(s): **25**

**Emissions Unit Details**

1. Package Unit:	
Manufacturer: <b>General Electric</b>	Model Number: <b>7FA</b>
2. Generator Nameplate Rating: <b>174 MW</b>	
3. Incinerator Information:	
Dwell Temperature:	°F
Dwell Time:	seconds
Incinerator Afterburner Temperature:	°F

**Emissions Unit Control Equipment**

1. Control Equipment/Method Description (Limit to 200 characters per device or method):

**Water injection - distillate oil firing**

2. Control Device or Method Code(s): **28**

**Emissions Unit Details**

1. Package Unit:		
Manufacturer: <b>General Electric</b>	Model Number: <b>7FA</b>	
2. Generator Nameplate Rating:	<b>183 MW</b>	
3. Incinerator Information:		
Dwell Temperature:		°F
Dwell Time:		seconds
Incinerator Afterburner Temperature:		°F

**B. EMISSIONS UNIT CAPACITY INFORMATION  
(Regulated Emissions Units Only)**

**Emissions Unit Operating Capacity and Schedule**

1. Maximum Heat Input Rate:	<b>1,614</b>	mmBtu/hr
2. Maximum Incineration Rate:	lb/hr	tons/day
3. Maximum Process or Throughput Rate:		
4. Maximum Production Rate:		
5. Requested Maximum Operating Schedule:		
	hours/day	days/week
	weeks/year	<b>3,390</b> hours/year
6. Operating Capacity/Schedule Comment (limit to 200 characters):		
<p><b>Maximum heat input at ISO conditions and natural gas firing (LHV); maximum for oil firing is 1,790 MMBtu/hr (ISO-LHV) and 183 MW.</b></p>		



**C. EMISSIONS UNIT REGULATIONS  
(Regulated Emissions Units Only)**

**List of Applicable Regulations**

See Attachment PRS-EU1-D for operational requirements	
See Attachment PSD-PRS for permitting requirements	

## ATTACHMENT PRS-EU1-D

### Applicable Requirements Listing

EMISSION UNIT ID: EU1

#### FDEP Rules:

##### Air Pollution Control-General Provisions:

62-204.800(7)(b)37. (State Only)	NSPS Subpart GG
62-204.800(7)(c) (State Only)	NSPS authority
62-204.800(7)(d)(State Only)	NSPS General Provisions
62-204.800(12) (State Only)	Acid Rain Program
62-204.800(13) (State Only)	Allowances
62-204.800(14) (State Only)	Acid Rain Program Monitoring
62-204.800(16) (State Only)	Excess Emissions (Potentially applicable over term of permit)

##### Stationary Sources-General:

62-210.650	Circumvention; EUs with control device
62-210.700(1)	Excess Emissions;
62-210.700(4)	Excess Emissions; poor maintenance
62-210.700(6)	Excess Emissions; notification

##### Acid Rain:

62-214.300	All Acid Rain Units (Applicability)
62-214.320(1)(a),(2)	All Acid Rain Units (Application Shield)
62-214.330(1)(a)1.	Compliance Options (if 214.430)
62-214.340	Exemptions (new units, retired units)
62-214.350(2);(3);(6)	All Acid Rain Units (Certification)
62-214.370	All Acid Rain Units (Revisions; correction; potentially applicable if a need arises)
62-214.430	All Acid Rain Units (Compliance Options-if required)

##### Stationary Sources-Emission Standards:

62-296.320(4)(b)(State Only)	CTs/Diesel Units
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##### Stationary Sources-Emission Monitoring (where stack test is required):

62-297.310(1)	All Units (Test Runs-Mass Emission)
62-297.310(2)(b)	All Units (Operating Rate; other than CTs;no CT)
62-297.310(3)	All Units (Calculation of Emission)
62-297.310(4)(a)	All Units (Applicable Test Procedures;Sampling time)
62-297.310(4)(b)	All Units (Sample Volume)
62-297.310(4)(c)	All Units (Required Flow Rate Range-PM/H2SO4/F)
62-297.310(4)(d)	All Units (Calibration)
62-297.310(4)(e)	All Units (EPA Method 5-only)

62-297.310(6)(a)	All Units (Permanent Test Facilities-general)
62-297.310(6)(c)	All Units (Sampling Ports)
62-297.310(6)(d)	All Units (Work Platforms)
62-297.310(6)(e)	All Units (Access)
62-297.310(6)(f)	All Units (Electrical Power)
62-297.310(6)(g)	All Units (Equipment Support)
62-297.310(7)(a)1.	Applies mainly to CTs/Diesels
62-297.310(7)(a)2.	FFSG excess emissions
62-297.310(7)(a)3.	Permit Renewal Test Required
62-297.310(7)(a)4.a	Annual Test
62-297.310(7)(a)5.	PM exemption if <400 hrs/yr
62-297.310(7)(a)6.	PM FFSG semi annual test required if >200 hrs/yr
62-297.310(7)(a)7.	PM quarterly monitoring if >100 hrs/yr
62-297.310(7)(a)9.	FDEP Notification - 15 days
62-297.310(7)(c)	Waiver of Compliance Tests (Fuel Sampling)
62-297.310(8)	Test Reports

#### Federal Rules:

##### NSPS Subpart GG:

40 CFR 60.332(a)(1)	NO <sub>x</sub> for Electric Utility CTs
40 CFR 60.332(a)(3)	NO <sub>x</sub> for Electric Utility CTs
40 CFR 60.333	SO <sub>2</sub> limits
40 CFR 60.334	Monitoring of Operations (Custom Monitoring for Gas)
40 CFR 60.335	Test Methods

##### NSPS General Requirements:

40 CFR 60.7(a)(1)	Notification of Construction
40 CFR 60.7(a)(2)	Notification of Initial Start-Up
40 CFR 60.7(a)(3)	Notification of Actual Start-Up
40 CFR 60.7(a)(4)	Notification and Recordkeeping (Physical/Operational Cycle)
40 CFR 60.7(a)(5)	Notification of CEM Demonstration
40 CFR 60.7(b)	Notification and Recordkeeping (startup/shutdown/malfunction)
40 CFR 60.7(c)	Notification and Recordkeeping (startup/shutdown/malfunction)
40 CFR 60.7(d)	Notification and Recordkeeping (startup/shutdown/malfunction)
40 CFR 60.7(f)	Notification and Recordkeeping (maintain records-2 yrs)
40 CFR 60.8(a)	Performance Test Requirements
40 CFR 60.8(b)	Performance Test Notification
40 CFR 60.8(c)	Performance Tests (representative conditions)
40 CFR 60.8(e)	Provide Stack Sampling Facilities
40 CFR 60.8(f)	Test Runs
40 CFR 60.11(a)	Compliance (ref. S. 60.8 or Subpart; other than opacity)
40 CFR 60.11(b)	Compliance (opacity determined EPA Method 9)
40 CFR 60.11(c)	Compliance (opacity; excludes startup/shutdown/malfunction)
40 CFR 60.11(d)	Compliance (maintain air pollution control equip.)
40 CFR 60.11(e)(2)	Compliance (opacity; ref. S. 60.8)
40 CFR 60.12	Circumvention

40 CFR 60.13(a)	Monitoring (Appendix B; Appendix F)
40 CFR 60.13(c)	Monitoring (Opacity COMS)
40 CFR 60.13(d)(1)	Monitoring (CEMS; span, drift, etc.)
40 CFR 60.13(d)(2)	Monitoring (COMS; span, system check)
40 CFR 60.13(e)	Monitoring (frequency of operation)
40 CFR 60.13(f)	Monitoring (frequency of operation)
40 CFR 60.13(h)	Monitoring (COMS; data requirements)
 Acid Rain-Permits:	
40 CFR 72.9(a)	Permit Requirements
40 CFR 72.9(b)	Monitoring Requirements
40 CFR 72.9(c)(1)	SO <sub>2</sub> Allowances-hold allowances
40 CFR 72.9(c)(2)	SO <sub>2</sub> Allowances-violation
40 CFR 72.9(c)(3)(iii)	SO <sub>2</sub> Allowances-Phase II Units (listed)
40 CFR 72.9(c)(4)	SO <sub>2</sub> Allowances-allowances held in ATS
40 CFR 72.9(c)(5)	SO <sub>2</sub> Allowances-no deduction for 72.9(c)(1)(i)
40 CFR 72.9(d)	NO <sub>x</sub> Requirements
40 CFR 72.9(e)	Excess Emission Requirements
40 CFR 72.9(f)	Recordkeeping and Reporting
40 CFR 72.9(g)	Liability
40 CFR 72.20(a)	Designated Representative; required
40 CFR 72.20(b)	Designated Representative; legally binding
40 CFR 72.20(c)	Designated Representative; certification requirements
40 CFR 72.21	Submissions
40 CFR 72.22	Alternate Designated Representative
40 CFR 72.23	Changing representatives; owners
40 CFR 72.24	Certificate of representation
40 CFR 72.30(a)	Requirements to Apply (operate)
40 CFR 72.30(b)(2)	Requirements to Apply (Phase II-Complete)
40 CFR 72.30(c)	Requirements to Apply (reapply before expiration)
40 CFR 72.30(d)	Requirements to Apply (submittal requirements)
40 CFR 72.31	Information Requirements; Acid Rain Applications
40 CFR 72.32	Permit Application Shield
40 CFR 72.33(b)	Dispatch System ID;unit/system ID
40 CFR 72.33(c)	Dispatch System ID;ID requirements
40 CFR 72.33(d)	Dispatch System ID;ID change
40 CFR 72.40(a)	General; compliance plan
40 CFR 72.40(b)	General; multi-unit compliance options
40 CFR 72.40(c)	General; conditional approval
40 CFR 72.40(d)	General; termination of compliance options
40 CFR 72.51	Permit Shield
40 CFR 72.90	Annual Compliance Certification
 Allowances:	
40 CFR 73.33(a),(c)	Authorized account representative
40 CFR 73.35(c)(1)	Compliance: ID of allowances by serial number

## Monitoring Part 75:

40 CFR 75.4	Compliance Dates;
40 CFR 75.5	Prohibitions
40 CFR 75.10(a)(1)	Primary Measurement; SO <sub>2</sub> ;
40 CFR 75.10(a)(2)	Primary Measurement; NO <sub>x</sub> ;
40 CFR 75.10(a)(3)(iii)	Primary Measurement; CO <sub>2</sub> ; O <sub>2</sub> monitor
40 CFR 75.10(b)	Primary Measurement; Performance Requirements
40 CFR 75.10(c)	Primary Measurement; Heat Input; Appendix F
40 CFR 75.10(e)	Primary Measurement; Optional Backup Monitor
40 CFR 75.10(f)	Primary Measurement; Minimum Measurement
40 CFR 75.10(g)	Primary Measurement; Minimum Recording
40 CFR 75.11(d)	SO <sub>2</sub> Monitoring; Gas- and Oil-fired units
40 CFR 75.11(e)	SO <sub>2</sub> Monitoring; Gaseous firing
40 CFR 75.12(a)	NO <sub>x</sub> Monitoring; Coal; Non-peaking oil/gas units
40 CFR 75.12(b)	NO <sub>x</sub> Monitoring; Determination of NO <sub>x</sub> emission rate; Appendix F
40 CFR 75.13(b)	CO <sub>2</sub> Monitoring; Appendix G
40 CFR 75.13(c)	CO <sub>2</sub> Monitoring; Appendix F
40 CFR 75.14(c)	Opacity Monitoring; Gas units; exemption
40 CFR 75.20(a)	Initial Certification Approval Process; Loss of Certification
40 CFR 75.20(b)	Recertification Procedures (if recertification necessary)
40 CFR 75.20(c)	Certification Procedures (if recertification necessary)
40 CFR 75.20(d)	Recertification Backup/portable monitor
40 CFR 75.20(f)	Alternate Monitoring system
40 CFR 75.21(a)	QA/QC; CEMS; Appendix B (Suspended 7/17/95-12/31/96)
40 CFR 75.21(c)	QA/QC; Calibration Gases
40 CFR 75.21(d)	QA/QC; Notification of RATA
40 CFR 75.21(e)	QA/QC; Audits
40 CFR 75.21(f)	QA/QC; CEMS (Effective 7/17/96-12/31/96)
40 CFR 75.22	Reference Methods
40 CFR 75.24	Out-of-Control Periods; CEMS
40 CFR 75.30(a)(3)	General Missing Data Procedures; NO <sub>x</sub>
40 CFR 75.30(a)(4)	General Missing Data Procedures; SO <sub>2</sub>
40 CFR 75.30(b)	General Missing Data Procedures; certified backup monitor
40 CFR 75.30(c)	General Missing Data Procedures; certified backup monitor
40 CFR 75.30(d)	General Missing Data Procedures; SO <sub>2</sub> (optional before 1/1/97)
40 CFR 75.30(e)	General Missing Data Procedures; bypass/multiple stacks
40 CFR 75.31	Initial Missing Data Procedures (new/re-certified CMS)
40 CFR 75.32	Monitoring Data Availability for Missing Data
40 CFR 75.33	Standard Missing Data Procedures
40 CFR 75.36	Missing Data for Heat Input
40 CFR 75.40	Alternate Monitoring Systems-General
40 CFR 75.41	Alternate Monitoring Systems-Precision Criteria
40 CFR 75.42	Alternate Monitoring Systems-Reliability Criteria
40 CFR 75.43	Alternate Monitoring Systems-Accessibility Criteria
40 CFR 75.44	Alternate Monitoring Systems-Timeliness Criteria
40 CFR 75.45	Alternate Monitoring Systems-Daily QA
40 CFR 75.46	Alternate Monitoring Systems-Missing data
40 CFR 75.47	Alternate Monitoring Systems-Criteria for Class

40 CFR 75.48	Alternate Monitoring Systems-Petition
40 CFR 75.53	Monitoring Plan; revisions
40 CFR 75.54(a)	Recordkeeping-general
40 CFR 75.54(b)	Recordkeeping-operating parameter
40 CFR 75.54(c)	Recordkeeping-SO <sub>2</sub>
40 CFR 75.54(d)	Recordkeeping- NO <sub>x</sub>
40 CFR 75.54(e)	Recordkeeping-CO <sub>2</sub>
40 CFR 75.54(f)	Recordkeeping-Opacity
40 CFR 75.55(c)	General Recordkeeping (Specific Situations)
40 CFR 75.55(e)	General Recordkeeping (Specific Situations)
40 CFR 75.56	Certification; QA/QC Provisions
40 CFR 75.60	Reporting Requirements-General
40 CFR 75.61	Reporting Requirements-Notification cert/recertification
40 CFR 75.62	Reporting Requirements-Monitoring Plan
40 CFR 75.63	Reporting Requirements-Certification/Recertification
40 CFR 75.64(a)	Reporting Requirements-Quarterly reports; submission
40 CFR 75.64(b)	Reporting Requirements-Quarterly reports; DR statement
40 CFR 75.64(c)	Rep. Req.; Quarterly reports; Compliance Certification
40 CFR 75.64(d)	Rep. Req.; Quarterly reports; Electronic format
40 CFR 75.66	Petitions to the Administrator (if required)
Appendix A-1	Installation and Measurement Locations
Appendix A-2.	Equipment Specifications
Appendix A-3.	Performance Specifications
Appendix A-4.	Data Handling and Acquisition Systems
Appendix A-5.	Calibration Gases
Appendix A-6.	Certification Tests and Procedures
Appendix A-7.	Calculations
Appendix B	QA/QC Procedures
Appendix C-1.	Missing Data; SO <sub>2</sub> / NO <sub>x</sub> for controlled sources
Appendix C-2.	Missing Data; Load-Based Procedure; NO <sub>x</sub> & flow
Appendix D	Optional SO <sub>2</sub> ; Oil-/gas-fired units
Appendix F	Conversion Procedures
Appendix H	Traceability Protocol

Acid Rain Program-Excess Emissions (these are future requirements):

40 CFR 77.3	Offset Plans (future)
40 CFR 77.5(b)	Deductions of Allowances (future)
40 CFR 77.6	Excess Emissions Penalties (SO <sub>2</sub> and NO <sub>x</sub> ;future)

**D. EMISSION POINT (STACK/VENT) INFORMATION  
(Regulated Emissions Units Only)**

**Emission Point Description and Type**

1. Identification of Point on Plot Plan or Flow Diagram? <b>See Att. PSD-PRS</b>		2. Emission Point Type Code: <b>1</b>	
3. Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking (limit to 100 characters per point):  <b>Exhausts through a single stack.</b>			
4. ID Numbers or Descriptions of Emission Units with this Emission Point in Common:			
5. Discharge Type Code: <b>V</b>	6. Stack Height: <b>60 feet</b>	7. Exit Diameter: <b>21 feet</b>	
8. Exit Temperature: <b>1,097 °F</b>	9. Actual Volumetric Flow Rate: <b>2,375,800 acfm</b>	10. Water Vapor: <b>8.7 %</b>	
11. Maximum Dry Standard Flow Rate: <b>725,000 dscfm</b>		12. Nonstack Emission Point Height: <b>feet</b>	
13. Emission Point UTM Coordinates:  Zone: <b>17</b> East (km): <b>419.5</b> North (km): <b>3069.7</b>			
14. Emission Point Comment (limit to 200 characters):  <b>Stack parameters for ISO operating condition firing natural gas; for oil 1,078°F and 2,443,200 ACFM.</b>			

**E. SEGMENT (PROCESS/FUEL) INFORMATION**  
**(All Emissions Units)**

**Segment Description and Rate:** Segment  1  of  2

1. Segment Description (Process/Fuel Type) (limit to 500 characters):  <b>Distillate (No. 2) Fuel Oil</b>		
2. Source Classification Code (SCC): <b>20100101</b>		3. SCC Units: <b>1,000 gallons used</b>
4. Maximum Hourly Rate: <b>14.1</b>	5. Maximum Annual Rate: <b>9,776</b>	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur: <b>0.05</b>	8. Maximum % Ash:	9. Million Btu per SCC Unit: <b>132</b>
10. Segment Comment (limit to 200 characters):  <b>Million Btu per SCC Unit = 131.8 (rounded to 132). Based on 7.1 lb/gal; LHV of 18,560 Btu/lb, ISO conditions, 720 hrs/yr operation.</b>		

**Segment Description and Rate:** Segment  2  of  2

1. Segment Description (Process/Fuel Type ) (limit to 500 characters):  <b>Natural Gas</b>		
2. Source Classification Code (SCC): <b>20100201</b>		3. SCC Units: <b>Million Cubic Feet</b>
4. Maximum Hourly Rate: <b>1.82</b>	5. Maximum Annual Rate: <b>5,947</b>	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur:	8. Maximum % Ash:	9. Million Btu per SCC Unit: <b>920</b>
10. Segment Comment (limit to 200 characters):  <b>Based on 920 Btu/cf (LHV); ISO conditions and 3,390 hrs/yr operation.</b>		





**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>PM</b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>22</b> lb/hour <b>22.6</b> tons/year	4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing, all loads. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>22 lb/hr</b>	4. Equivalent Allowable Emissions: <b>22 lb/hour      7.9 tons/year</b>
5. Method of Compliance (limit to 60 characters):  <b>Annual stack test; EPA Methods 5 or 17; if &lt; 400 hours</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing - all loads; 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>PM</b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>22</b> lb/hour <b>22.6</b> tons/year	4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; all loads. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>11 lb/hr</b>	4. Equivalent Allowable Emissions: <b>11 lb/hour      18.6 tons/year</b>
5. Method of Compliance (limit to 60 characters):  <b>VE Test &lt; 20% opacity</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Gas firing - all loads; 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>SO<sub>2</sub></b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>106.9 lb/hour      50.5 tons/year</b>		4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]	
5. Range of Estimated Fugitive Emissions: [ ] 1 [ ] 2 [ ] 3 _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000, Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Emission Factor: 2 grains S per 100 CF gas; 0.05% S oil lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>0.05% Sulfur Oil</b>		4. Equivalent Allowable Emissions: <b>106.9 lb/hour      37.2 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>Fuel Sampling</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing; max @ 32°F; 100% load;TPY @ 59°F, 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>SO<sub>2</sub></b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>106.9 lb/hour</b>		4. Synthetically Limited? <input checked="" type="checkbox"/> [ X ]	
		<b>50.5 tons/year</b>	
5. Range of Estimated Fugitive Emissions: [ ] 1 [ ] 2 [ ] 3 _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Emission Factor: 2 grains S per 100 CF gas; 0.05% S oil lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>See Comment</b>		4. Equivalent Allowable Emissions: <b>10.4 lb/hour 17.0 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>Fuel Sampling</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Requested allowable emissions and units: Pipeline Natural Gas. Gas firing, 2 grains S/100 cf - 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>NO<sub>x</sub></b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>352 lb/hour                      215 tons/year</b>	4. Synthetically Limited? <input checked="" type="checkbox"/>
5. Range of Estimated Fugitive Emissions: [ ] 1            [ ] 2            [ ] 3            _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>42 ppmvd</b>	4. Equivalent Allowable Emissions: <b>352 lb/hour                      122 tons/year</b>
5. Method of Compliance (limit to 60 characters):  <b>CEM - 30 Day Rolling Average</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Requested Allowable Emissions is at 15% O<sub>2</sub>-100% load. Oil firing; max @ 32°F; 100% load; TPY @ 59°F, 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION  
(Regulated Emissions Units -  
Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>NO<sub>x</sub></b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>352 lb/hour      215 tons/year</b>		4. Synthetically Limited? <input checked="" type="checkbox"/>	
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>10 ppmvd</b>		4. Equivalent Allowable Emissions: <b>71.9 lb/hour      117.4 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>CEM - 30 Day Rolling Average</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Requested Allowable Emissions and Units is at 15% O<sub>2</sub>-100% load. Gas firing; 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>CO</b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>72.6</b> lb/hour <b>70.8</b> tons/year	4. Synthetically Limited? <input checked="" type="checkbox"/>
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions</b>	

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>20 ppmvd</b>	4. Equivalent Allowable Emissions: <b>72.6</b> lb/hour <b>25.0</b> tons/year
5. Method of Compliance (limit to 60 characters):  <b>EPA Method 10; high and low load</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing; max @ 32°F; 100% load; TPY @ 59°F, 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	



**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION  
(Regulated Emissions Units -  
Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>CO</b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>72.6</b> lb/hour		4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]	
		<b>70.8</b> tons/year	
5. Range of Estimated Fugitive Emissions: [ ] 1 [ ] 2 [ ] 3 _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>10 ppmvd</b>		4. Equivalent Allowable Emissions: <b>35.9</b> lb/hour <b>58.1</b> tons/year	
5. Method of Compliance (limit to 60 characters):  <b>EPA Method 10; high and low load</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Gas firing; 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>VOC</b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>8.1</b> lb/hour <b>8.2</b> tons/year	4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>4 ppmvd</b>	4. Equivalent Allowable Emissions: <b>8.1</b> lb/hour <b>2.8</b> tons/year
5. Method of Compliance (limit to 60 characters):  <b>EPA Method 25A; high and low load</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing; max @ 32°F; 100% load; TPY @ 59°F, 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION  
(Regulated Emissions Units -  
Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>VOC</b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>8.1</b> lb/hour <b>8.2</b> tons/year		4. Synthetically Limited? <input checked="" type="checkbox"/>	
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>2.0 ppmvd</b>		4. Equivalent Allowable Emissions: <b>4.2 lb/hour      6.9 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>EPA Method 25A; high and low load</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Additional requested allowable emissions and units: Gas firing; 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>PM<sub>10</sub></b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>22 lb/hour                      22.6 tons/year</b>	4. Synthetically Limited? <input checked="" type="checkbox"/>
5. Range of Estimated Fugitive Emissions: [ ] 1            [ ] 2            [ ] 3            _____ to _____ tons/year	
6. Emission Factor: <b>Reference: GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 59°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions</b>	

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>22 lb/hr</b>	4. Equivalent Allowable Emissions: <b>22 lb/hour                      7.9 tons/year</b>
5. Method of Compliance (limit to 60 characters):  <b>Annual stack test; EPA Method 5 or 17; if &lt;400 hours</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing - all loads; 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>PM<sub>10</sub></b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>22 lb/hour                      22.6 tons/year</b>	4. Synthetically Limited? <input checked="" type="checkbox"/>
5. Range of Estimated Fugitive Emissions: [ ] 1            [ ] 2            [ ] 3            _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 59°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>11 lb/hr</b>	4. Equivalent Allowable Emissions: <b>11 lb/hour                      18.6 tons/year</b>
5. Method of Compliance (limit to 60 characters):  <b>VE Test &lt; 20% opacity</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Gas firing; all loads; 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	



**H. VISIBLE EMISSIONS INFORMATION**  
**(Only Regulated Emissions Units Subject to a VE Limitation)**

**Visible Emissions Limitation:** Visible Emissions Limitation 2 of 2

1. Visible Emissions Subtype: <b>VE99</b>	2. Basis for Allowable Opacity: <input checked="" type="checkbox"/> Rule <input type="checkbox"/> Other
3. Requested Allowable Opacity: Normal Conditions:      %      Exceptional Conditions: <b>100 %</b> Maximum Period of Excess Opacity Allowed: <b>6 min/hour</b>	
4. Method of Compliance: <b>None</b>	
5. Visible Emissions Comment (limit to 200 characters):  <b>FDEP Rule 62-201.700(1), Allowed for 2 hours (120 minutes) per 24 hours for start up, shutdown and malfunction.</b>	

**I. CONTINUOUS MONITOR INFORMATION**  
**(Only Regulated Emissions Units Subject to Continuous Monitoring)**

**Continuous Monitoring System:** Continuous Monitor 2 of 2

1. Parameter Code: <b>EM</b>	2. Pollutant(s): <b>NO<sub>x</sub></b>
3. CMS Requirement: <input checked="" type="checkbox"/> Rule <input type="checkbox"/> Other	
4. Monitor Information: <b>Not yet determined</b> Manufacturer: Model Number:      Serial Number:	
5. Installation Date: <b>01 Jun 2002</b>	6. Performance Specification Test Date:
7. Continuous Monitor Comment (limit to 200 characters):  <b>Parameter Code: WTF. Required by 40 CFR Part 60; subpart GG; 60.334.</b>	

**J. EMISSIONS UNIT SUPPLEMENTAL INFORMATION**  
**(Regulated Emissions Units Only)**

**Supplemental Requirements**

1. Process Flow Diagram <input checked="" type="checkbox"/> Attached, Document ID: <u>PSD-PRS</u> [   ] Not Applicable [   ] Waiver Requested
2. Fuel Analysis or Specification <input checked="" type="checkbox"/> Attached, Document ID: <u>PSD-PRS</u> [   ] Not Applicable [   ] Waiver Requested
3. Detailed Description of Control Equipment <input checked="" type="checkbox"/> Attached, Document ID: <u>PSD-PRS</u> [   ] Not Applicable [   ] Waiver Requested
4. Description of Stack Sampling Facilities <input checked="" type="checkbox"/> Attached, Document ID: <u>PSD-PRS</u> [   ] Not Applicable [   ] Waiver Requested
5. Compliance Test Report <input type="checkbox"/> Attached, Document ID: _____ <input type="checkbox"/> Previously submitted, Date: _____ <input checked="" type="checkbox"/> Not Applicable
6. Procedures for Startup and Shutdown <input type="checkbox"/> Attached, Document ID: _____ <input checked="" type="checkbox"/> Not Applicable [   ] Waiver Requested
7. Operation and Maintenance Plan <input type="checkbox"/> Attached, Document ID: _____ <input checked="" type="checkbox"/> Not Applicable [   ] Waiver Requested
8. Supplemental Information for Construction Permit Application <input checked="" type="checkbox"/> Attached, Document ID: <u>PSD-PRS</u> [   ] Not Applicable
9. Other Information Required by Rule or Statute <input checked="" type="checkbox"/> Attached, Document ID: <u>PSD-PRS</u> [   ] Not Applicable
10. Supplemental Requirements Comment:          



**Additional Supplemental Requirements for Title V Air Operation Permit Applications**

## 11. Alternative Methods of Operation

 Attached, Document ID: \_\_\_\_\_  Not Applicable

## 12. Alternative Modes of Operation (Emissions Trading)

 Attached, Document ID: \_\_\_\_\_  Not Applicable

## 13. Identification of Additional Applicable Requirements

 Attached, Document ID: \_\_\_\_\_  Not Applicable

## 14. Compliance Assurance Monitoring Plan

 Attached, Document ID: \_\_\_\_\_  Not Applicable

## 15. Acid Rain Part Application (Hard-copy Required)

 Acid Rain Part - Phase II (Form No. 62-210.900(1)(a))  
Attached, Document ID: \_\_\_\_\_ Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)  
Attached, Document ID: \_\_\_\_\_ New Unit Exemption (Form No. 62-210.900(1)(a)2.)  
Attached, Document ID: \_\_\_\_\_ Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)  
Attached, Document ID: \_\_\_\_\_ Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)  
Attached, Document ID: \_\_\_\_\_ Phase NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)  
Attached, Document ID: \_\_\_\_\_ Not Applicable

**III. EMISSIONS UNIT INFORMATION**

A separate Emissions Unit Information Section (including subsections A through J as required) must be completed for each emissions unit addressed in this Application for Air Permit. If submitting the application form in hard copy, indicate, in the space provided at the top of each page, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application.

**A. GENERAL EMISSIONS UNIT INFORMATION  
(All Emissions Units)**

**Emissions Unit Description and Status**

<p>1. Type of Emissions Unit Addressed in This Section: (Check one)</p> <p><input checked="" type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).</p> <p><input type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.</p> <p><input type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only.</p>			
<p>2. Regulated or Unregulated Emissions Unit? (Check one)</p> <p><input checked="" type="checkbox"/> The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.</p> <p><input type="checkbox"/> The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.</p>			
<p>3. Description of Emissions Unit Addressed in This Section (limit to 60 characters): <b>GE Frame 7FA Combustion Turbine</b></p>			
<p>4. Emissions Unit Identification Number: <span style="float: right;"><input type="checkbox"/> No ID</span></p> <p>ID: <span style="float: right;"><input checked="" type="checkbox"/> ID Unknown</span></p>			
<p>5. Emissions Unit Status Code: <b>C</b></p>	<p>6. Initial Startup Date:</p>	<p>7. Emissions Unit Major Group SIC Code: <b>49</b></p>	<p>8. Acid Rain Unit? <input checked="" type="checkbox"/></p>
<p>9. Emissions Unit Comment: (Limit to 500 Characters)</p> <p><b>This emission unit is a GE Frame 7FA combustion turbine operating in simple cycle mode. See Attachment PSD-PRS.</b></p>			

**Emissions Unit Control Equipment**

1. Control Equipment/Method Description (Limit to 200 characters per device or method):

**Dry Low NO<sub>x</sub> combustion - Natural gas firing**

2. Control Device or Method Code(s): **25**

**Emissions Unit Details**

1. Package Unit:		
Manufacturer:	<b>General Electric</b>	Model Number: <b>7FA</b>
2. Generator Nameplate Rating: <b>174 MW</b>		
3. Incinerator Information:		
	Dwell Temperature:	°F
	Dwell Time:	seconds
	Incinerator Afterburner Temperature:	°F

**Emissions Unit Control Equipment**

1. Control Equipment/Method Description (Limit to 200 characters per device or method):

**Water injection - distillate oil firing**

2. Control Device or Method Code(s): **28**

**Emissions Unit Details**

1. Package Unit:

Manufacturer: **General Electric**

Model Number: **7FA**

2. Generator Nameplate Rating:

**183** MW

3. Incinerator Information:

Dwell Temperature:

°F

Dwell Time:

seconds

Incinerator Afterburner Temperature:

°F

**B. EMISSIONS UNIT CAPACITY INFORMATION  
(Regulated Emissions Units Only)**

**Emissions Unit Operating Capacity and Schedule**

1. Maximum Heat Input Rate:	<b>1,614</b>	mmBtu/hr
2. Maximum Incineration Rate:	lb/hr	tons/day
3. Maximum Process or Throughput Rate:		
4. Maximum Production Rate:		
5. Requested Maximum Operating Schedule:		
	hours/day	days/week
	weeks/year	<b>3,390</b> hours/year
6. Operating Capacity/Schedule Comment (limit to 200 characters):		
<p><b>Maximum heat input at ISO conditions and natural gas firing (LHV); maximum for oil firing is 1,790 MMBtu/hr (ISO-LHV) and 183 MW.</b></p>		



**D. EMISSION POINT (STACK/VENT) INFORMATION  
(Regulated Emissions Units Only)**

**Emission Point Description and Type**

1. Identification of Point on Plot Plan or Flow Diagram? <b>See Att. PSD-PRS</b>		2. Emission Point Type Code: <b>1</b>	
3. Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking (limit to 100 characters per point):  <b>Exhausts through a single stack.</b>			
4. ID Numbers or Descriptions of Emission Units with this Emission Point in Common:			
5. Discharge Type Code: <b>V</b>	6. Stack Height: <b>60 feet</b>	7. Exit Diameter: <b>22 feet</b>	
8. Exit Temperature: <b>1,113 °F</b>	9. Actual Volumetric Flow Rate: <b>2,375,800 acfm</b>	10. Water Vapor: <b>8.7 %</b>	
11. Maximum Dry Standard Flow Rate: <b>725,000 dscfm</b>		12. Nonstack Emission Point Height: <b>feet</b>	
13. Emission Point UTM Coordinates:  Zone: <b>17</b> East (km): <b>419.5</b> North (km): <b>3069.7</b>			
14. Emission Point Comment (limit to 200 characters):  <b>Stack parameters for ISO operating condition firing natural gas; for oil 1,078°F and 2,443,200 ACFM.</b>			

**E. SEGMENT (PROCESS/FUEL) INFORMATION**  
(All Emissions Units)

**Segment Description and Rate:** Segment 1 of 2

1. Segment Description (Process/Fuel Type) (limit to 500 characters):  <b>Distillate (No. 2) Fuel Oil</b>		
2. Source Classification Code (SCC): <b>20100101</b>		3. SCC Units: <b>1,000 gallons used</b>
4. Maximum Hourly Rate: <b>14.1</b>	5. Maximum Annual Rate: <b>9,776</b>	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur: <b>0.05</b>	8. Maximum % Ash:	9. Million Btu per SCC Unit: <b>132</b>
10. Segment Comment (limit to 200 characters):  <b>Million Btu per SCC Unit = 131.8 (rounded to 132). Based on 7.1 lb/gal; LHV of 18,560 Btu/lb, ISO conditions, 720 hrs/yr operation.</b>		

**Segment Description and Rate:** Segment 2 of 2

1. Segment Description (Process/Fuel Type ) (limit to 500 characters):  <b>Natural Gas</b>		
2. Source Classification Code (SCC): <b>20100201</b>		3. SCC Units: <b>Million Cubic Feet</b>
4. Maximum Hourly Rate: <b>1.82</b>	5. Maximum Annual Rate: <b>5,947</b>	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur:	8. Maximum % Ash:	9. Million Btu per SCC Unit: <b>920</b>
10. Segment Comment (limit to 200 characters):  <b>Based on 920 Btu/cf (LHV); ISO conditions and 3,390 hrs/yr operation.</b>		





**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>PM</b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>22 lb/hour      22.6 tons/year</b>	4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; all loads. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>11 lb/hr</b>	4. Equivalent Allowable Emissions: <b>11 lb/hour      18.6 tons/year</b>
5. Method of Compliance (limit to 60 characters):  <b>VE Test &lt; 20% opacity</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Gas firing - all loads; 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>PM</b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>22</b> lb/hour <b>22.6</b> tons/year	4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing, all loads. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>22 lb/hr</b>	4. Equivalent Allowable Emissions: <b>22 lb/hour      7.9 tons/year</b>
5. Method of Compliance (limit to 60 characters):  <b>Annual stack test; EPA Methods 5 or 17; if &lt; 400 hours</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing - all loads; 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>SO<sub>2</sub></b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>106.9 lb/hour      50.5 tons/year</b>	4. Synthetically Limited? <input checked="" type="checkbox"/>
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000, Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Emission Factor: 2 grains S per 100 CF gas; 0.05% S oil lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>0.05% Sulfur Oil</b>	4. Equivalent Allowable Emissions: <b>106.9 lb/hour      37.2 tons/year</b>
5. Method of Compliance (limit to 60 characters):  <b>Fuel Sampling</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing; max @ 32°F; 100% load;TPY @ 59°F, 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>SO<sub>2</sub></b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>106.9 lb/hour      50.5 tons/year</b>		4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]	
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year			
6. Emission Factor: <b>Reference: GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Emission Factor: 2 grains S per 100 CF gas; 0.05% S oil lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>See Comment</b>		4. Equivalent Allowable Emissions: <b>10.4 lb/hour      17.0 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>Fuel Sampling</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Requested allowable emissions and units: Pipeline Natural Gas. Gas firing, 2 grains S/100 cf - 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION  
(Regulated Emissions Units -  
Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>NO<sub>x</sub></b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>352 lb/hour                      215 tons/year</b>		4. Synthetically Limited? <input checked="" type="checkbox"/>	
5. Range of Estimated Fugitive Emissions: [ ] 1            [ ] 2            [ ] 3            _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>42 ppmvd</b>		4. Equivalent Allowable Emissions: <b>352 lb/hour                      122 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>CEM - 30 Day Rolling Average</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Requested Allowable Emissions is at 15% O<sub>2</sub>-100% load. Oil firing; max @ 32°F; 100% load; TPY @ 59°F, 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION  
(Regulated Emissions Units -  
Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>NO<sub>x</sub></b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>352 lb/hour      215 tons/year</b>		4. Synthetically Limited? <input checked="" type="checkbox"/>	
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>10 ppmvd</b>		4. Equivalent Allowable Emissions: <b>71.9 lb/hour      117.4 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>CEM - 30 Day Rolling Average</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Requested Allowable Emissions and Units is at 15% O<sub>2</sub>-100% load. Gas firing; 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION  
(Regulated Emissions Units -  
Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>CO</b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>72.6</b> lb/hour <b>70.8</b> tons/year		4. Synthetically Limited? <input checked="" type="checkbox"/>	
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions</b>			

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>20 ppmvd</b>		4. Equivalent Allowable Emissions: <b>72.6</b> lb/hour <b>25.0</b> tons/year	
5. Method of Compliance (limit to 60 characters):  <b>EPA Method 10; high and low load</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing; max @ 32°F; 100% load; TPY @ 59°F, 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			



**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION  
(Regulated Emissions Units -  
Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>CO</b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>72.6</b> lb/hour <b>70.8</b> tons/year		4. Synthetically Limited? <input checked="" type="checkbox"/>	
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>10 ppmvd</b>		4. Equivalent Allowable Emissions: <b>35.9</b> lb/hour <b>58.1</b> tons/year	
5. Method of Compliance (limit to 60 characters):  <b>EPA Method 10; high and low load</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Gas firing; 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>VOC</b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>8.1</b> lb/hour <b>8.2</b> tons/year	4. Synthetically Limited? <input checked="" type="checkbox"/>
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>4 ppmvd</b>	4. Equivalent Allowable Emissions: <b>8.1 lb/hour      2.8 tons/year</b>
5. Method of Compliance (limit to 60 characters):  <b>EPA Method 25A; high and low load</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing; max @ 32°F; 100% load; TPY @ 59°F, 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>VOC</b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>8.1</b> lb/hour <b>8.2</b> tons/year	4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>2.0 ppmvd</b>	4. Equivalent Allowable Emissions: <b>4.2</b> lb/hour <b>6.9</b> tons/year
5. Method of Compliance (limit to 60 characters):  <b>EPA Method 25A; high and low load</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Additional requested allowable emissions and units: Gas firing; 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>PM<sub>10</sub></b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>22 lb/hour                      22.6 tons/year</b>		4. Synthetically Limited? <input checked="" type="checkbox"/>	
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 59°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>22 lb/hr</b>		4. Equivalent Allowable Emissions: <b>22 lb/hour                      7.9 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>Annual stack test; EPA Method 5 or 17; if &lt;400 hours</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing - all loads; 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>PM<sub>10</sub></b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>22 lb/hour                      22.6 tons/year</b>	4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]
5. Range of Estimated Fugitive Emissions: [ ] 1            [ ] 2            [ ] 3            _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 59°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>11 lb/hr</b>	4. Equivalent Allowable Emissions: <b>11 lb/hour                      18.6 tons/year</b>
5. Method of Compliance (limit to 60 characters):  <b>VE Test &lt; 20% opacity</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Gas firing; all loads; 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**H. VISIBLE EMISSIONS INFORMATION**  
**(Only Regulated Emissions Units Subject to a VE Limitation)**

**Visible Emissions Limitation:** Visible Emissions Limitation 1 of 2

1. Visible Emissions Subtype: <b>VE20</b>	2. Basis for Allowable Opacity: <input checked="" type="checkbox"/> Rule <input type="checkbox"/> Other
3. Requested Allowable Opacity: Normal Conditions: <b>20 %</b> Exceptional Conditions: <b>        </b> % Maximum Period of Excess Opacity Allowed: <b>        </b> min/hour	
4. Method of Compliance: <b>Annual VE Test EPA Method 9</b>	
5. Visible Emissions Comment (limit to 200 characters):  <b>Maximum for oil firing.</b>	

**I. CONTINUOUS MONITOR INFORMATION**  
**(Only Regulated Emissions Units Subject to Continuous Monitoring)**

**Continuous Monitoring System:** Continuous Monitor 1 of 2

1. Parameter Code: <b>EM</b>	2. Pollutant(s): <b>NO<sub>x</sub></b>
3. CMS Requirement:	<input checked="" type="checkbox"/> Rule <input type="checkbox"/> Other
4. Monitor Information: <b>Not yet determined</b> Manufacturer: Model Number: <b>        </b> Serial Number: <b>        </b>	
5. Installation Date: <b>01 Jun 2002</b>	6. Performance Specification Test Date:
7. Continuous Monitor Comment (limit to 200 characters):  <b>NO<sub>x</sub> CEM proposed to meet requirements of 40 CFR Part 75.</b>	



**J. EMISSIONS UNIT SUPPLEMENTAL INFORMATION  
(Regulated Emissions Units Only)****Supplemental Requirements**

1. Process Flow Diagram [ <b>X</b> ] Attached, Document ID: <u>PSD-PRS</u> [ ] Not Applicable [ ] Waiver Requested
2. Fuel Analysis or Specification [ <b>X</b> ] Attached, Document ID: <u>PSD-PRS</u> [ ] Not Applicable [ ] Waiver Requested
3. Detailed Description of Control Equipment [ <b>X</b> ] Attached, Document ID: <u>PSD-PRS</u> [ ] Not Applicable [ ] Waiver Requested
4. Description of Stack Sampling Facilities [ <b>X</b> ] Attached, Document ID: <u>PSD-PRS</u> [ ] Not Applicable [ ] Waiver Requested
5. Compliance Test Report [ ] Attached, Document ID: _____ [ ] Previously submitted, Date: _____ [ <b>X</b> ] Not Applicable
6. Procedures for Startup and Shutdown [ ] Attached, Document ID: _____ [ <b>X</b> ] Not Applicable [ ] Waiver Requested
7. Operation and Maintenance Plan [ ] Attached, Document ID: _____ [ <b>X</b> ] Not Applicable [ ] Waiver Requested
8. Supplemental Information for Construction Permit Application [ <b>X</b> ] Attached, Document ID: <u>PSD-PRS</u> [ ] Not Applicable
9. Other Information Required by Rule or Statute [ <b>X</b> ] Attached, Document ID: <u>PSD-PRS</u> [ ] Not Applicable
10. Supplemental Requirements Comment:



**Additional Supplemental Requirements for Title V Air Operation Permit Applications**

## 11. Alternative Methods of Operation

 Attached, Document ID: \_\_\_\_\_  Not Applicable

## 12. Alternative Modes of Operation (Emissions Trading)

 Attached, Document ID: \_\_\_\_\_  Not Applicable

## 13. Identification of Additional Applicable Requirements

 Attached, Document ID: \_\_\_\_\_  Not Applicable

## 14. Compliance Assurance Monitoring Plan

 Attached, Document ID: \_\_\_\_\_  Not Applicable

## 15. Acid Rain Part Application (Hard-copy Required)

 Acid Rain Part - Phase II (Form No. 62-210.900(1)(a))

Attached, Document ID: \_\_\_\_\_

 Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)

Attached, Document ID: \_\_\_\_\_

 New Unit Exemption (Form No. 62-210.900(1)(a)2.)

Attached, Document ID: \_\_\_\_\_

 Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)

Attached, Document ID: \_\_\_\_\_

 Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)

Attached, Document ID: \_\_\_\_\_

 Phase NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)

Attached, Document ID: \_\_\_\_\_

 Not Applicable

**III. EMISSIONS UNIT INFORMATION**

A separate Emissions Unit Information Section (including subsections A through J as required) must be completed for each emissions unit addressed in this Application for Air Permit. If submitting the application form in hard copy, indicate, in the space provided at the top of each page, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application.

**A. GENERAL EMISSIONS UNIT INFORMATION  
(All Emissions Units)**

**Emissions Unit Description and Status**

1. Type of Emissions Unit Addressed in This Section: (Check one)			
<input checked="" type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).			
<input type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.			
<input type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only.			
2. Regulated or Unregulated Emissions Unit? (Check one)			
<input checked="" type="checkbox"/> The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.			
<input type="checkbox"/> The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.			
3. Description of Emissions Unit Addressed in This Section (limit to 60 characters): <b>GE Frame 7FA Combustion Turbine</b>			
4. Emissions Unit Identification Number: <span style="float:right">[ ] No ID</span>			
ID: <span style="float:right">[ X ] ID Unknown</span>			
5. Emissions Unit Status Code: <b>C</b>	6. Initial Startup Date:	7. Emissions Unit Major Group SIC Code: <b>49</b>	8. Acid Rain Unit? <input checked="" type="checkbox"/>
9. Emissions Unit Comment: (Limit to 500 Characters)			
<b>This emission unit is a GE Frame 7FA combustion turbine operating in simple cycle mode. See Attachment PSD-PRS.</b>			

**Emissions Unit Control Equipment**

1. Control Equipment/Method Description (Limit to 200 characters per device or method):

**Dry Low NO<sub>x</sub> combustion - Natural gas firing**

2. Control Device or Method Code(s): **25**

**Emissions Unit Details**

1. Package Unit:

Manufacturer: **General Electric**

Model Number: **7FA**

2. Generator Nameplate Rating:

**174 MW**

3. Incinerator Information:

Dwell Temperature:

°F

Dwell Time:

seconds

Incinerator Afterburner Temperature:

°F

**Emissions Unit Control Equipment**

1. Control Equipment/Method Description (Limit to 200 characters per device or method):

**Water injection - distillate oil firing**

2. Control Device or Method Code(s): **28**

**Emissions Unit Details**

1. Package Unit:

Manufacturer: **General Electric**

Model Number: **7FA**

2. Generator Nameplate Rating:

**183 MW**

3. Incinerator Information:

Dwell Temperature:

°F

Dwell Time:

seconds

Incinerator Afterburner Temperature:

°F

**B. EMISSIONS UNIT CAPACITY INFORMATION  
(Regulated Emissions Units Only)**

**Emissions Unit Operating Capacity and Schedule**

1. Maximum Heat Input Rate:	<b>1,614</b>	mmBtu/hr
2. Maximum Incineration Rate:	lb/hr	tons/day
3. Maximum Process or Throughput Rate:		
4. Maximum Production Rate:		
5. Requested Maximum Operating Schedule:		
	hours/day	days/week
	weeks/year	<b>3,390</b> hours/year
6. Operating Capacity/Schedule Comment (limit to 200 characters):		
<p><b>Maximum heat input at ISO conditions and natural gas firing (LHV); maximum for oil firing is 1,790 MMBtu/hr (ISO-LHV) and 183 MW.</b></p>		

**C. EMISSIONS UNIT REGULATIONS  
(Regulated Emissions Units Only)**

**List of Applicable Regulations**

See Attachment PRS-EU1-D for operational requirements	
See Attachment PSD-PRS for permitting requirements	

**D. EMISSION POINT (STACK/VENT) INFORMATION**  
**(Regulated Emissions Units Only)**

**Emission Point Description and Type**

1. Identification of Point on Plot Plan or Flow Diagram? <b>See Att. PSD-PRS</b>		2. Emission Point Type Code: <b>1</b>	
3. Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking (limit to 100 characters per point):  <b>Exhausts through a single stack.</b>			
4. ID Numbers or Descriptions of Emission Units with this Emission Point in Common:			
5. Discharge Type Code: <b>V</b>	6. Stack Height: <b>60</b> feet	7. Exit Diameter: <b>21</b> feet	
8. Exit Temperature: <b>1,097</b> °F	9. Actual Volumetric Flow Rate: <b>2,375,800</b> acfm	10. Water Vapor: <b>8.7</b> %	
11. Maximum Dry Standard Flow Rate: <b>725,000</b> dscfm		12. Nonstack Emission Point Height: feet	
13. Emission Point UTM Coordinates: Zone: <b>17</b> East (km): <b>419.5</b> North (km): <b>3069.7</b>			
14. Emission Point Comment (limit to 200 characters):  <b>Stack parameters for ISO operating condition firing natural gas; for oil 1,078°F and 2,443,200 ACFM.</b>			

**E. SEGMENT (PROCESS/FUEL) INFORMATION**  
**(All Emissions Units)**

**Segment Description and Rate:** Segment  1  of  2

1. Segment Description (Process/Fuel Type) (limit to 500 characters):  <b>Distillate (No. 2) Fuel Oil</b>		
2. Source Classification Code (SCC): <b>20100101</b>		3. SCC Units: <b>1,000 gallons used</b>
4. Maximum Hourly Rate: <b>14.1</b>	5. Maximum Annual Rate: <b>9,776</b>	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur: <b>0.05</b>	8. Maximum % Ash:	9. Million Btu per SCC Unit: <b>132</b>
10. Segment Comment (limit to 200 characters):  <b>Million Btu per SCC Unit = 131.8 (rounded to 132). Based on 7.1 lb/gal; LHV of 18,560 Btu/lb, ISO conditions, 720 hrs/yr operation.</b>		

**Segment Description and Rate:** Segment  2  of  2

1. Segment Description (Process/Fuel Type ) (limit to 500 characters):  <b>Natural Gas</b>		
2. Source Classification Code (SCC): <b>20100201</b>		3. SCC Units: <b>Million Cubic Feet</b>
4. Maximum Hourly Rate: <b>1.82</b>	5. Maximum Annual Rate: <b>5,947</b>	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur:	8. Maximum % Ash:	9. Million Btu per SCC Unit: <b>920</b>
10. Segment Comment (limit to 200 characters):  <b>Based on 920 Btu/cf (LHV); ISO conditions and 3,390 hrs/yr operation.</b>		





**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION  
(Regulated Emissions Units -  
Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>PM</b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>22</b> lb/hour <b>22.6</b> tons/year		4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]	
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing, all loads. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>22 lb/hr</b>		4. Equivalent Allowable Emissions: <b>22 lb/hour      7.9 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>Annual stack test; EPA Methods 5 or 17; if &lt; 400 hours</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing - all loads; 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>PM</b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>22</b> lb/hour <b>22.6</b> tons/year		4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]	
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; all loads. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>11 lb/hr</b>		4. Equivalent Allowable Emissions: <b>11 lb/hour      18.6 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>VE Test &lt; 20% opacity</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Gas firing - all loads; 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>SO<sub>2</sub></b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>106.9 lb/hour      50.5 tons/year</b>		4. Synthetically Limited? <input checked="" type="checkbox"/>	
5. Range of Estimated Fugitive Emissions: [ ] 1 [ ] 2 [ ] 3 _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000, Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Emission Factor: 2 grains S per 100 CF gas; 0.05% S oil lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>0.05% Sulfur Oil</b>		4. Equivalent Allowable Emissions: <b>106.9 lb/hour      37.2 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>Fuel Sampling</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing; max @ 32°F; 100% load;TPY @ 59°F, 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>SO<sub>2</sub></b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>106.9 lb/hour      50.5 tons/year</b>		4. Synthetically Limited? <input checked="" type="checkbox"/>	
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Emission Factor: 2 grains S per 100 CF gas; 0.05% S oil lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>See Comment</b>		4. Equivalent Allowable Emissions: <b>10.4 lb/hour      17.0 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>Fuel Sampling</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Requested allowable emissions and units: Pipeline Natural Gas. Gas firing, 2 grains S/100 cf - 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>NO<sub>x</sub></b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>352 lb/hour                      215 tons/year</b>	4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3                      to                      tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>42 ppmvd</b>	4. Equivalent Allowable Emissions: <b>352 lb/hour                      122 tons/year</b>
5. Method of Compliance (limit to 60 characters):  <b>CEM - 30 Day Rolling Average</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Requested Allowable Emissions is at 15% O<sub>2</sub>-100% load. Oil firing; max @ 32°F; 100% load; TPY @ 59°F, 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION  
(Regulated Emissions Units -  
Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>NO<sub>x</sub></b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>352</b> lb/hour <b>215</b> tons/year		4. Synthetically Limited? <input checked="" type="checkbox"/>	
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>10 ppmvd</b>		4. Equivalent Allowable Emissions: <b>71.9 lb/hour      117.4 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>CEM - 30 Day Rolling Average</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Requested Allowable Emissions and Units is at 15% O<sub>2</sub>-100% load. Gas firing; 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>CO</b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>72.6</b> lb/hour <b>70.8</b> tons/year	4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions</b>	

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>20 ppmvd</b>	4. Equivalent Allowable Emissions: <b>72.6</b> lb/hour <b>25.0</b> tons/year
5. Method of Compliance (limit to 60 characters):  <b>EPA Method 10; high and low load</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing; max @ 32°F; 100% load; TPY @ 59°F, 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	



**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>CO</b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>72.6</b> lb/hour <b>70.8</b> tons/year	4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>10 ppmvd</b>	4. Equivalent Allowable Emissions: <b>35.9</b> lb/hour <b>58.1</b> tons/year
5. Method of Compliance (limit to 60 characters):  <b>EPA Method 10; high and low load</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Gas firing; 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>VOC</b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>8.1</b> lb/hour <b>8.2</b> tons/year	4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>4 ppmvd</b>	4. Equivalent Allowable Emissions: <b>8.1</b> lb/hour <b>2.8</b> tons/year
5. Method of Compliance (limit to 60 characters):  <b>EPA Method 25A; high and low load</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing; max @ 32°F; 100% load; TPY @ 59°F, 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION  
(Regulated Emissions Units -  
Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>VOC</b>		2. Total Percent Efficiency of Control:	
3. Potential Emissions: <b>8.1</b> lb/hour <b>8.2</b> tons/year		4. Synthetically Limited? [ <input checked="" type="checkbox"/> ]	
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year			
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>		7. Emissions Method Code: <b>2</b>	
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>			

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: <b>2.0 ppmvd</b>		4. Equivalent Allowable Emissions: <b>4.2 lb/hour      6.9 tons/year</b>	
5. Method of Compliance (limit to 60 characters):  <b>EPA Method 25A; high and low load</b>			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Additional requested allowable emissions and units: Gas firing; 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>			

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>PM<sub>10</sub></b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>22 lb/hour                      22.6 tons/year</b>	4. Synthetically Limited? <input checked="" type="checkbox"/>
5. Range of Estimated Fugitive Emissions: [ ] 1      [ ] 2      [ ] 3      _____ to _____ tons/year	
6. Emission Factor: Reference: <b>GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 59°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>22 lb/hr</b>	4. Equivalent Allowable Emissions: <b>22 lb/hour                      7.9 tons/year</b>
5. Method of Compliance (limit to 60 characters):  <b>Annual stack test; EPA Method 5 or 17; if &lt;400 hours</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Oil firing - all loads; 720 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**  
**(Regulated Emissions Units -**  
**Emissions-Limited and Preconstruction Review Pollutants Only)**

**Potential/Fugitive Emissions**

1. Pollutant Emitted: <b>PM<sub>10</sub></b>	2. Total Percent Efficiency of Control:
3. Potential Emissions: <b>22 lb/hour                      22.6 tons/year</b>	4. Synthetically Limited? <input checked="" type="checkbox"/>
5. Range of Estimated Fugitive Emissions: [ ] 1            [ ] 2            [ ] 3            _____ to _____ tons/year	
6. Emission Factor: <b>Reference: GE, 2000; Decker</b>	7. Emissions Method Code: <b>2</b>
8. Calculation of Emissions (limit to 600 characters):  <b>See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters):  <b>Lb/hr based on oil firing; 100% load; 59°F. Tons/yr based on 2,670 hrs/yr gas firing and 720 hrs/yr oil firing; ISO conditions.</b>	

**Allowable Emissions** Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: <b>OTHER</b>	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: <b>11 lb/hr</b>	4. Equivalent Allowable Emissions: <b>11 lb/hour                      18.6 tons/year</b>
5. Method of Compliance (limit to 60 characters):  <b>VE Test &lt; 20% opacity</b>	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters):  <b>Gas firing; all loads; 3,390 hrs/yr. See Attachment PSD-PRS; Section 2.0; Appendix A.</b>	

**H. VISIBLE EMISSIONS INFORMATION**  
**(Only Regulated Emissions Units Subject to a VE Limitation)**

**Visible Emissions Limitation:** Visible Emissions Limitation 1 of 2

1. Visible Emissions Subtype: <b>VE20</b>	2. Basis for Allowable Opacity: <input checked="" type="checkbox"/> Rule <input type="checkbox"/> Other
3. Requested Allowable Opacity: Normal Conditions: <b>20 %</b> Exceptional Conditions:      % Maximum Period of Excess Opacity Allowed:      min/hour	
4. Method of Compliance: <b>Annual VE Test EPA Method 9</b>	
5. Visible Emissions Comment (limit to 200 characters):  <b>Maximum for oil firing.</b>	

**I. CONTINUOUS MONITOR INFORMATION**  
**(Only Regulated Emissions Units Subject to Continuous Monitoring)**

**Continuous Monitoring System:** Continuous Monitor 1 of 2

1. Parameter Code: <b>EM</b>	2. Pollutant(s): <b>NO<sub>x</sub></b>
3. CMS Requirement: <input checked="" type="checkbox"/> Rule <input type="checkbox"/> Other	
4. Monitor Information: <b>Not yet determined</b> Manufacturer: Model Number:      Serial Number:	
5. Installation Date: <b>01 Jun 2002</b>	6. Performance Specification Test Date:
7. Continuous Monitor Comment (limit to 200 characters):  <b>NO<sub>x</sub> CEM proposed to meet requirements of 40 CFR Part 75.</b>	



**J. EMISSIONS UNIT SUPPLEMENTAL INFORMATION  
(Regulated Emissions Units Only)****Supplemental Requirements**

1. Process Flow Diagram [ <b>X</b> ] Attached, Document ID: <u>PSD-PRS</u> [ ] Not Applicable [ ] Waiver Requested
2. Fuel Analysis or Specification [ <b>X</b> ] Attached, Document ID: <u>PSD-PRS</u> [ ] Not Applicable [ ] Waiver Requested
3. Detailed Description of Control Equipment [ <b>X</b> ] Attached, Document ID: <u>PSD-PRS</u> [ ] Not Applicable [ ] Waiver Requested
4. Description of Stack Sampling Facilities [ <b>X</b> ] Attached, Document ID: <u>PSD-PRS</u> [ ] Not Applicable [ ] Waiver Requested
5. Compliance Test Report [ ] Attached, Document ID: _____ [ ] Previously submitted, Date: _____ [ <b>X</b> ] Not Applicable
6. Procedures for Startup and Shutdown [ ] Attached, Document ID: _____ [ <b>X</b> ] Not Applicable [ ] Waiver Requested
7. Operation and Maintenance Plan [ ] Attached, Document ID: _____ [ <b>X</b> ] Not Applicable [ ] Waiver Requested
8. Supplemental Information for Construction Permit Application [ <b>X</b> ] Attached, Document ID: <u>PSD-PRS</u> [ ] Not Applicable
9. Other Information Required by Rule or Statute [ <b>X</b> ] Attached, Document ID: <u>PSD-PRS</u> [ ] Not Applicable
10. Supplemental Requirements Comment:



**Additional Supplemental Requirements for Title V Air Operation Permit Applications**

11. Alternative Methods of Operation [ ] Attached, Document ID: _____ [ ] Not Applicable
12. Alternative Modes of Operation (Emissions Trading) [ ] Attached, Document ID: _____ [ ] Not Applicable
13. Identification of Additional Applicable Requirements [ ] Attached, Document ID: _____ [ ] Not Applicable
14. Compliance Assurance Monitoring Plan [ ] Attached, Document ID: _____ [ ] Not Applicable
15. Acid Rain Part Application (Hard-copy Required) [ ] Acid Rain Part - Phase II (Form No. 62-210.900(1)(a)) Attached, Document ID: _____ [ ] Repowering Extension Plan (Form No. 62-210.900(1)(a)1.) Attached, Document ID: _____ [ ] New Unit Exemption (Form No. 62-210.900(1)(a)2.) Attached, Document ID: _____ [ ] Retired Unit Exemption (Form No. 62-210.900(1)(a)3.) Attached, Document ID: _____ [ ] Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.) Attached, Document ID: _____ [ ] Phase NOx Averaging Plan (Form No. 62-210.900(1)(a)5.) Attached, Document ID: _____ [ ] Not Applicable

**III. EMISSIONS UNIT INFORMATION**

A separate Emissions Unit Information Section (including subsections A through J as required) must be completed for each emissions unit addressed in this Application for Air Permit. If submitting the application form in hard copy, indicate, in the space provided at the top of each page, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application.

**A. GENERAL EMISSIONS UNIT INFORMATION  
(All Emissions Units)**

**Emissions Unit Description and Status**

<p>1. Type of Emissions Unit Addressed in This Section: (Check one)</p> <p><input type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).</p> <p><input checked="" type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.</p> <p><input type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only.</p>			
<p>2. Regulated or Unregulated Emissions Unit? (Check one)</p> <p><input type="checkbox"/> The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.</p> <p><input checked="" type="checkbox"/> The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.</p>			
<p>3. Description of Emissions Unit Addressed in This Section (limit to 60 characters):</p> <p><b>Unreg. Emissions Activities - 2 Tanks at 1.5 M gallons each</b></p>			
<p>4. Emissions Unit Identification Number:</p> <p>ID:</p>		<p><input type="checkbox"/> No ID</p> <p><input checked="" type="checkbox"/> ID Unknown</p>	
<p>5. Emissions Unit Status Code:</p> <p><b>C</b></p>	<p>6. Initial Startup Date:</p>	<p>7. Emissions Unit Major Group SIC Code:</p> <p><b>49</b></p>	<p>8. Acid Rain Unit?</p> <p><input type="checkbox"/></p>
<p>9. Emissions Unit Comment: (Limit to 500 Characters)</p> <p><b>This emission unit information section addresses two 1.5 million gallon tanks as unregulated emission units. NSPS Subpart Kb recordkeeping requirements are applicable; there is no emission limiting or work practice standards. See Attachment PSD-PRS.</b></p>			



**E. SEGMENT (PROCESS/FUEL) INFORMATION**  
**(All Emissions Units)**

**Segment Description and Rate:** Segment 1 of 1

1. Segment Description (Process/Fuel Type) (limit to 500 characters):  <b>No. 2 Distillate Oil/Diesel</b>		
2. Source Classification Code (SCC): <b>A2505030090</b>		3. SCC Units: <b>1,000 gallons used</b>
4. Maximum Hourly Rate:	5. Maximum Annual Rate: <b>29,340</b>	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur:	8. Maximum % Ash:	9. Million Btu per SCC Unit: <b>132</b>
10. Segment Comment (limit to 200 characters):  <b>Annual rate combined for both tanks based on inputs to CTs; 18,560 Btu/lb (LHV); and 7.1 lb/gal at 59°F.</b>		

**Segment Description and Rate:** Segment      of     

1. Segment Description (Process/Fuel Type) (limit to 500 characters):		
2. Source Classification Code (SCC):		3. SCC Units:
4. Maximum Hourly Rate:	5. Maximum Annual Rate:	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur:	8. Maximum % Ash:	9. Million Btu per SCC Unit:
10. Segment Comment (limit to 200 characters):		



**PART B**

**REPORT**

## 1.0 INTRODUCTION

Peace River Station, L.L.C. proposes to license, construct, and operate a nominal 525-megawatt (MW) power production facility, referred to as the Peace River Station (the "Project"), in the City of Fort Meade, Polk County, Florida (Figure 1-1). The site will be located on a 31.55-acre tract. The Project consists of three 175-MW dual-fuel, General Electric Frame 7FA combustion turbines (CTs) that will use dry low-nitrogen oxide (NO<sub>x</sub>) (DLN) combustion technology when operating on natural gas and water injection (for NO<sub>x</sub> control) when operating on distillate fuel oil. The facility is designed for peaking service. The primary fuel for the combustion turbines will be natural gas with distillate fuel oil used as backup fuel. Fuel oil will contain a maximum sulfur content of 0.05 percent.

The permitting of the Project in Florida requires an air construction permit and prevention of significant deterioration (PSD) review approval. To assist in performing the necessary licensing activities, Peace River Station, L.L.C. has contracted Golder Associates Inc. (Golder) to perform the necessary air quality assessments for determining the Project's compliance with state and federal new source review (NSR) regulation, including PSD and nonattainment review requirements. The critical aspects of these assessments include the air quality impact analyses performed using an air dispersion model and the best available control technology (BACT) analyses performed to evaluate the selected emission control technology.

The proposed Project will be a new air pollution source that will result in increases in air emissions in Polk County. The U.S. Environmental Protection Agency (EPA) has implemented regulations requiring a PSD review. PSD regulations are promulgated under Volume 40 Code of Federal Regulations (CFR) Part 52.21 and implemented through delegation to the Florida Department of Environmental Protection (DEP). Florida's PSD regulations are codified in Rules 62-212.400, F.A.C. These regulations incorporate the EPA PSD regulations.

Based on the emissions from the proposed Project, a PSD review is required for each of the following regulated pollutants:

- Particulate matter (PM) as total suspended particulate matter (TSP),
- Particulate matter with aerodynamic diameter of 10 microns or less (PM<sub>10</sub>),
- Nitrogen dioxide (NO<sub>2</sub>),
- Sulfur dioxide (SO<sub>2</sub>),
- Carbon monoxide (CO), and
- Sulfuric acid mist.

Polk County has been designated as an attainment area for all criteria pollutants [i.e., attainment: ozone (O<sub>3</sub>), PM<sub>10</sub>, SO<sub>2</sub>, CO, and NO<sub>2</sub>; unclassifiable: lead] and is classified as a PSD Class II area for PM<sub>10</sub>, SO<sub>2</sub>, and NO<sub>2</sub>; therefore, the PSD review will follow regulations pertaining to such designations.

The air permit application is divided into seven major sections.

- Section 2.0 presents a description of the facility, including air emissions and stack parameters.
- Section 3.0 provides a review of the PSD and nonattainment requirements applicable to the proposed Project.
- Section 4.0 includes the control technology review with discussions on BACT.
- Section 5.0 discusses the ambient air monitoring analysis (pre-construction monitoring) required by PSD regulations.
- Section 6.0 presents a summary of the air modeling approach and results used in assessing compliance of the proposed Project with ambient air quality standards (AAQS), PSD increments, and good engineering practice (GEP) stack height regulations.
- Section 7.0 provides the additional impact analyses for soils, vegetation, and visibility.



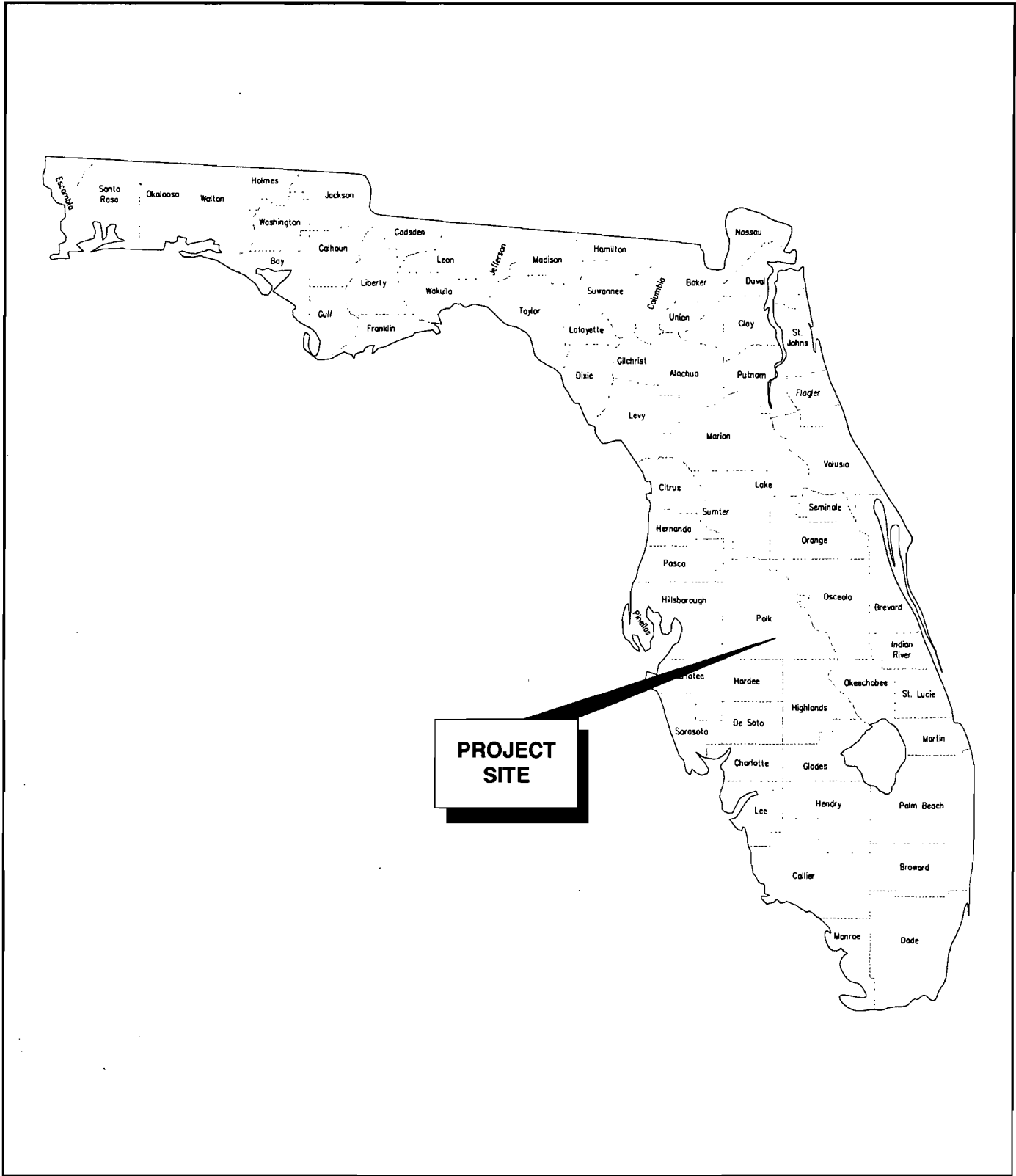


Figure 1-1. General Site Location



## 2.0 PROJECT DESCRIPTION

### 2.1 SITE DESCRIPTION

The Project site, shown in Figure 2-1, consists of about 31.55 acres that are currently agricultural. There is industrial, commercial, and residential development within a 3-kilometer (km) radius of the site; however, this development is located about 0.8 km (0.5 miles) to the east in the City of Fort Meade. The plant elevation will be approximately 130 feet above sea level. The terrain surrounding the site is flat.

The Project will connect to the electrical grid at the existing Florida Power Corporation (FPC) Fort Meade Substation located adjacent to and west of the southwest boundary of the site. The Project will likely connect to an existing natural gas pipeline lateral from the Florida Gas Transmission Company's (FGT) transmission pipeline or one of two proposed new pipelines to be located near the site. Natural gas will be transported to the site via a new pipeline lateral to be constructed to the site. Distillate fuel oil will be delivered by truck and stored in tanks located at the plant site.

Water for the NO<sub>x</sub> control when firing oil will be supplied by the City of Fort Meade. Potable water and additional fire protection supply water will be served by the City of Fort Meade.

### 2.2 POWER PLANT

The proposed Project will consist of three General Electric Frame 7FA CTs and associated facilities. The annual maximum capacity factor of the plant will be 39 percent, which is equivalent to operating 3,390 hours per year at full load. Natural gas will be used as the primary fuel, and fuel oil will be used as a backup fuel. Fuel oil usage will be limited to the equivalent of 720 hours per year at full load.

Plant performance with General Electric 7FA combustion turbines was developed for natural gas and oil; at 50-, 75-, and 100-percent load; and at 32°F, 59°F, and 95°F turbine inlet temperatures. Combustion turbine performance is based on a performance envelope developed from General Electric.

The CTs will be capable of normal steady state operation from 50 to 100 percent of baseload. The efficiency of the CTs decreases at part load. As a result, the economic incentive is to dispatch the plant to keep the units operating as near baseload as possible.

Natural gas will be transported to the site via pipeline and fuel oil will be trucked to the site. The distillate fuel oil, which will have a maximum sulfur content of 0.05 percent, will be stored onsite in two aboveground storage tanks, each sized to hold approximately 35,714 barrels (1.5 million gallons).

Air emissions control will consist of using state-of-the-art dry low-NO<sub>x</sub> burners in the CTs when firing natural gas. The General Electric Frame 7FA will be equipped with the General Electric dry low-NO<sub>x</sub> (DLN- NO<sub>x</sub>) combustion system that regulates the distribution of fuel delivery to a multi-nozzle, total premix combustor arrangement. The fuel flow distribution to each combustion system fuel nozzle is regulated to maintain unit load and optimum turbine emissions. Water injection will be used for NO<sub>x</sub> control when firing distillate fuel oil. The SO<sub>2</sub> emissions will be controlled by the use of low-sulfur fuels. Good combustion practices and clean fuels will also minimize potential emissions of PM, CO, VOC, and other pollutants (e.g., trace metals). These engineering and environmental designs maximize control of air emissions while minimizing economic, environmental, and energy impacts (see Section 4.0 for the BACT evaluation).

### **2.3 PROPOSED SOURCE EMISSIONS AND STACK PARAMETERS**

The estimated maximum hourly emissions and exhaust information representative of the proposed CT design operating at baseload conditions (100-percent load), 75-percent load and 50-percent load conditions are presented in Tables 2-1 and 2-2. The information is

presented in these tables for one unit simple cycle operation based on natural gas combustion and fuel oil combustion. The data are presented for turbine inlet temperatures of 32°F, 59°F, and 95°F. These temperatures represent the range of ambient temperatures that the CTs are most likely to experience.

The performance calculations for the operating conditions are given in Appendix A.

The pollutant gaseous emission concentrations and  $PM_{10}$  emission rates for the proposed CTs at baseload conditions and ambient temperature of 59 °F are as follows:

Pollutant	Natural Gas	Distillate Oil
$NO_x$ , ppmvd @ 15% $O_2$	9	42
CO, ppmvd	10	20
VOC as $CH_4$ , ppmvd @ 15% $O_2$	2.0	2.8
$SO_x$ as $SO_2$	Calculated Based on Fuel (2.0 grains S/100 SCF)	Calculated Based on Fuel (0.05% sulfur)
$PM_{10}$ lb/hr (dry filterable)	11	22

The maximum short-term emission rates (lb/hr) generally occur at baseload, 32°F operation, where the CT has the greatest output and greatest fuel consumption.

Based on a turbine inlet temperature of 59°F, the emission rates used to calculate maximum potential annual emissions for the proposed facility for regulated air pollutants for one and three CTs are presented in Table 2-3. To produce the maximum annual emissions, the CTs are assumed to operate at baseload for 3,390 hours (39 percent capacity factor) firing natural gas for 2,670 hours and fuel oil for 720 hours. The potential emissions are based on the 59°F turbine inlet air condition since it represents a nominal average between the higher emission levels at the 32°F turbine inlet condition (winter) and the infrequent 95°F turbine inlet condition (summer). A summary of the maximum potential annual emissions for the Project is presented in Table 2-4 and the Project's emissions are compared to the PSD significant emission rates. As shown, the Project's emissions are major for  $NO_x$  and greater than the significant emission rates for  $SO_2$ , PM,  $PM_{10}$ , CO, and sulfuric acid mist.

Process flow diagrams of the turbine operating at turbine inlet temperature of 32°F, 59°F, and 95°F are presented in Figures 2-2 through 2-4, respectively for the CT.

Based on a review of the emission rates for natural gas and fuel oil combustion, the highest emission rates for the regulated pollutants generally occur when firing fuel oil. Combustion of natural gas and fuel oil result in slightly different exhaust flow gas rates and stack exit temperatures; however, the differences are minor.

As discussed in Section 6.0, the air modeling analyses that addressed compliance with ambient standards were based on modeling the CTs for the operating load and ambient temperature which produced the maximum impacts from the load impact analysis that was performed. Although the highest emission rates occur with low turbine inlet temperatures (i.e., 32°F) and baseload conditions, the lowest exhaust gas flow rates occur with a turbine inlet temperature of 95°F and 50 percent operating load. Since this low exhaust flow condition can result in potentially higher impacts due to lower plume rise (i.e., due to lower exit velocity and temperature), the load analysis included modeling the CTs for the following six scenarios designed to determine the maximum impacts for the Project:

- Base operating load for the turbine inlet temperatures of 32°F and 95°F;
- A 75-percent operating load for the turbine inlet temperatures of 32°F and 95°F; and
- A 50-percent operating load for the turbine inlet temperatures of 32°F and 95°F.

#### **2.4 SITE LAYOUT, STRUCTURES, AND STACK SAMPLING FACILITIES**

The plot plan of the proposed facility is presented in Figure 2-5. The dimensions of the buildings and structures are presented in Section 6.0. Stack sampling facilities will be constructed in accordance to Rule 62-297.310(6) F.A.C.

The plot plan shows facility property lines, major process equipment and structures, and all emission points. The entrance to the site will have security gates to control site access. The fenced property boundary is shown in the figure.

Table 2-1. Stack, Operating, and Emission Data for Simple Cycle Combustion Turbine  
Natural Gas Firing

Parameter	Operating and Emission Data <sup>a</sup> for Ambient Temperature			
	32 °F	59 °F	75 °F	95 °F
<u>Stack Data (ft)</u>				
Height	60	60	60	60
Diameter	21	21	21	21
<u>100 Percent Load</u>				
Operating Data				
Temperature (°F)	1,076	1,097	1,115	1,124
Velocity (ft/sec)	118.6	115.8	112.4	110.4
Maximum Hourly Emissions per Unit <sup>b</sup>				
SO <sub>2</sub> lb/hr	10.4	10.0	9.5	9.3
PM/PM10 lb/hr	11.0	11.0	11.0	11.0
NO <sub>x</sub> lb/hr	71.9	69.3	65.7	63.9
CO lb/hr	35.9	34.3	32.4	31.4
VOC (as methane) lb/hr	4.2	4.1	3.9	3.8
Sulfuric Acid Mist lb/hr	2.39	2.30	2.19	2.13
Mercury lb/hr	1.49E-06	1.43E-06	1.36E-06	1.32E-06
<u>75 Percent Load</u>				
Operating Data				
Temperature (°F)	1,164	1,179	1,180	1,180
Velocity (ft/sec)	100.1	96.7	94.6	91.7
Maximum Hourly Emissions per Unit <sup>b</sup>				
SO <sub>2</sub> lb/hr	8.6	8.1	7.8	7.3
PM/PM10 lb/hr	11.0	11.0	11.0	11.0
NO <sub>x</sub> lb/hr	59.3	55.9	53.7	50.6
CO lb/hr	28.5	27.2	26.2	25.3
VOC (as methane) lb/hr	3.4	3.2	3.1	3.1
Sulfuric Acid Mist lb/hr	1.97	1.86	1.79	1.68
Mercury lb/hr	1.23E-06	1.16E-06	1.11E-06	1.05E-06
<u>50 Percent Load</u>				
Operating Data				
Temperature (°F)	1,076	1,048	1,049	1,052
Velocity (ft/sec)	82.9	81.0	79.7	78.0
Maximum Hourly Emissions per Unit <sup>b</sup>				
SO <sub>2</sub> lb/hr	6.5	6.1	5.9	5.6
PM/PM10 lb/hr	11.0	11.0	11.0	11.0
NO <sub>x</sub> lb/hr	44.7	42.1	40.6	38.5
CO lb/hr	25.2	25.1	24.3	23.6
VOC (as methane) lb/hr	3.0	3.0	2.8	2.8
Sulfuric Acid Mist lb/hr	1.49	1.40	1.35	1.28
Mercury lb/hr	9.28E-07	8.72E-07	8.40E-07	7.97E-07

<sup>a</sup> Refer to Appendix A for detailed information. Data at 100% load for 95 °F are based on evaporative cooler on and operating at 95 percent efficiency.

<sup>b</sup> Other regulated pollutants are assumed to have negligible emissions. These pollutants include lead, reduced sulfur compounds, hydrogen sulfide, fluorides, MSW Organics, Metals and Acid Gases.

Basis for pollutant emission rates at 59 °F ambient temperature are:

SO<sub>2</sub> = 2.0 grain sulfur/ 100 cubic feet

PM/PM10 = dry filterables

NO<sub>x</sub> = 10.0 ppmvd at 15% O<sub>2</sub>

CO = 10.0 ppmvd

VOC = 2 ppmvd/100 and 75% load; 2.1 ppmvd at 50% load

Sulfuric acid mist = 15% SO<sub>2</sub> emissions

Mercury = Gas: 0.0008 lb/10<sup>12</sup> Btu.

Table 2-2. Stack, Operating, and Emission Data for the Simple Cycle Combustion Turbine  
Distillate Fuel Oil Firing

Parameter	Operating and Emission Data <sup>a</sup> for Ambient Temperature			
	32 °F	59 °F	75 °F	95 °F
<u>Stack Data (ft)</u>				
Height	60	60	60	60
Diameter	21	21	21	21
<u>100 Percent Load</u>				
Operating Data				
Temperature (°F)	1,054	1,078	1,101	1,111
Velocity (ft/sec)	121.7	119.1	116.0	114.0
Maximum Hourly Emissions per Unit <sup>b</sup>				
SO <sub>2</sub>	106.9	103.2	98.9	96.2
PM/PM10	22.0	22.0	22.0	22.0
NO <sub>x</sub>	352.1	340.1	326.0	316.9
CO	72.6	69.4	65.6	63.5
VOC (as methane)	8.1	7.8	7.5	7.3
Sulfuric Acid Mist	24.55	23.70	22.72	22.10
Mercury	1.23E-03	1.19E-03	1.14E-03	1.11E-03
<u>75 Percent Load</u>				
Operating Data				
Temperature (°F)	1,145	1,172	1,180	1,180
Velocity (ft/sec)	101.4	98.1	96.0	93.1
Maximum Hourly Emissions per Unit <sup>b</sup>				
SO <sub>2</sub>	87.2	83.0	79.9	75.3
PM/PM10	22.0	22.0	22.0	22.0
NO <sub>x</sub>	287.3	273.5	263.1	248.2
CO	56.9	53.8	51.6	50.0
VOC (as methane)	6.4	6.1	5.9	5.7
Sulfuric Acid Mist	20.03	19.06	18.35	17.30
Mercury	1.00E-03	9.56E-04	9.20E-04	8.67E-04
<u>50 Percent Load</u>				
Operating Data				
Temperature (°F)	1,040	1,018	1,020	1,025
Velocity (ft/sec)	83.6	81.9	80.6	78.9
Maximum Hourly Emissions per Unit <sup>b</sup>				
SO <sub>2</sub>	64.9	61.3	59.1	56.2
PM/PM10	22.0	22.0	22.0	22.0
NO <sub>x</sub>	213.9	201.8	194.8	185.2
CO	51.0	50.7	49.1	47.8
VOC (as methane)	5.6	5.6	5.5	5.4
Sulfuric Acid Mist	4.97	4.69	4.52	4.30
Mercury	7.47E-04	7.05E-04	6.80E-04	6.46E-04

<sup>a</sup> Refer to Appendix A for detailed information. Data at 100% load for 95 °F are based on evaporative cooler on and operating at 95 percent efficiency.

<sup>b</sup> Other regulated pollutants are assumed to have negligible and minor amounts of emissions. These pollutants include lead, reduced sulfur compounds, hydrogen sulfide, fluorides, MWC Organics, Metals and Acid Gases.

Basis for pollutant emission rates at 59 °F ambient temperature are:

SO<sub>2</sub> = 0.05% S in fuel oil

PM/PM10 = dry filterables

NO<sub>x</sub> = 42 ppmvd at 15% O<sub>2</sub>

CO = 20.1 ppmvd at 100 and 75% loads; 24.7 ppmvd at 50% load

VOC = 4 ppmvd at 100 and 75% loads; 4.7 ppmvd at 50% load

Sulfuric acid mist = 15% SO<sub>2</sub> emissions

Mercury = Oil: 0.626 lb/10<sup>12</sup> Btu

Table 2-3 Summary of Maximum Potential Annual Emissions for the Simple Cycle Combustion Turbine Project

Pollutant	Load: Fuel:	Hourly Emissions (lb/hr) <sup>a</sup>						Maximum Emissions (tons/year) <sup>b</sup>	
		100% Gas	75% Gas	50% Gas	100% Oil	75% Oil	50% Oil	Case A	Case B
<b>One Combustion Turbine- Simple Cycle</b>									
SO <sub>2</sub>		10.0	8.11	6.10	103	83.0	61.3	17.0	50.5
PM/PM10		11.0	11.0	11.0	22.0	22.0	22.0	18.6	22.6
NO <sub>x</sub>		69.3	55.9	42.1	340	274	202	117	215
CO		34.3	27.2	25	69.4	53.8	50.7	58.1	70.8
VOC (as methane)		4.05	3.24	2.97	7.80	6.10	5.60	6.9	8.2
Sulfuric Acid Mist		2.30	1.86	1.40	23.70	19.06	4.69	3.9	11.6
Mercury		1.43E-06	1.16E-06	8.72E-07	1.19E-03	9.56E-04	7.05E-04	2.4E-06	4.3E-04
Lead		NEG	NEG	NEG	7.38E-03	5.93E-03	4.38E-03	NEG	2.7E-03
Fluorides		NEG	NEG	NEG	2.22E-02	1.79E-02	1.32E-02	NEG	8.0E-03
MWC Organics (as 2,3,7,8-TCDD)		3.64E-09	2.95E-09	2.22E-09	2.60E-07	2.09E-07	1.54E-07	6.2E-09	9.8E-08
MWC Metals (as Be and Cd)		NEG	NEG	NEG	2.44E-03	1.96E-03	1.45E-03	NEG	8.8E-04
MWC Acid Gases (as HCl)		NEG	NEG	NEG	1.44E-01	1.16E-01	1.60E-08	NEG	5.2E-02
<b>Three Combustion Turbines- Simple Cycle</b>									
SO <sub>2</sub>		30.1	24.3	18.3	310	249	184	51.0	152
PM/PM10		33.0	33.0	33.0	66.0	66.0	66.0	55.9	67.8
NO <sub>x</sub>		208	168	126	1,020	821	605	352	645
CO		103	82	75	208	161	152	174	212
VOC (as methane)		12.2	9.72	8.91	23.4	18.3	16.8	20.6	24.6
Sulfuric Acid Mist		6.91	5.59	4.20	71.1	57.2	14.1	11.7	34.8
Mercury		4.30E-06	3.48E-06	2.62E-06	3.56E-03	2.87E-03	2.12E-03	7.29E-06	1.29E-03
Lead		NEG	NEG	NEG	2.2E-02	1.8E-02	1.3E-02	NEG	8.0E-03
Fluorides		NEG	NEG	NEG	6.7E-02	5.4E-02	4.0E-02	NEG	2.4E-02
MWC Organics (as 2,3,7,8-TCDD)		1.09E-08	8.85E-09	6.65E-09	7.8E-07	6.3E-07	4.6E-07	1.9E-08	2.9E-07
MWC Metals (as Be and Cd)		NEG	NEG	NEG	7.3E-03	5.9E-03	4.3E-03	NEG	2.6E-03
MWC Acid Gases (as HCl)		NEG	NEG	NEG	4.3E-01	3.5E-01	4.8E-08	NEG	1.6E-01

<sup>a</sup> Based on 59 °F ambient inlet air temperature. See Appendix A for details of emission factors used for each pollutant.

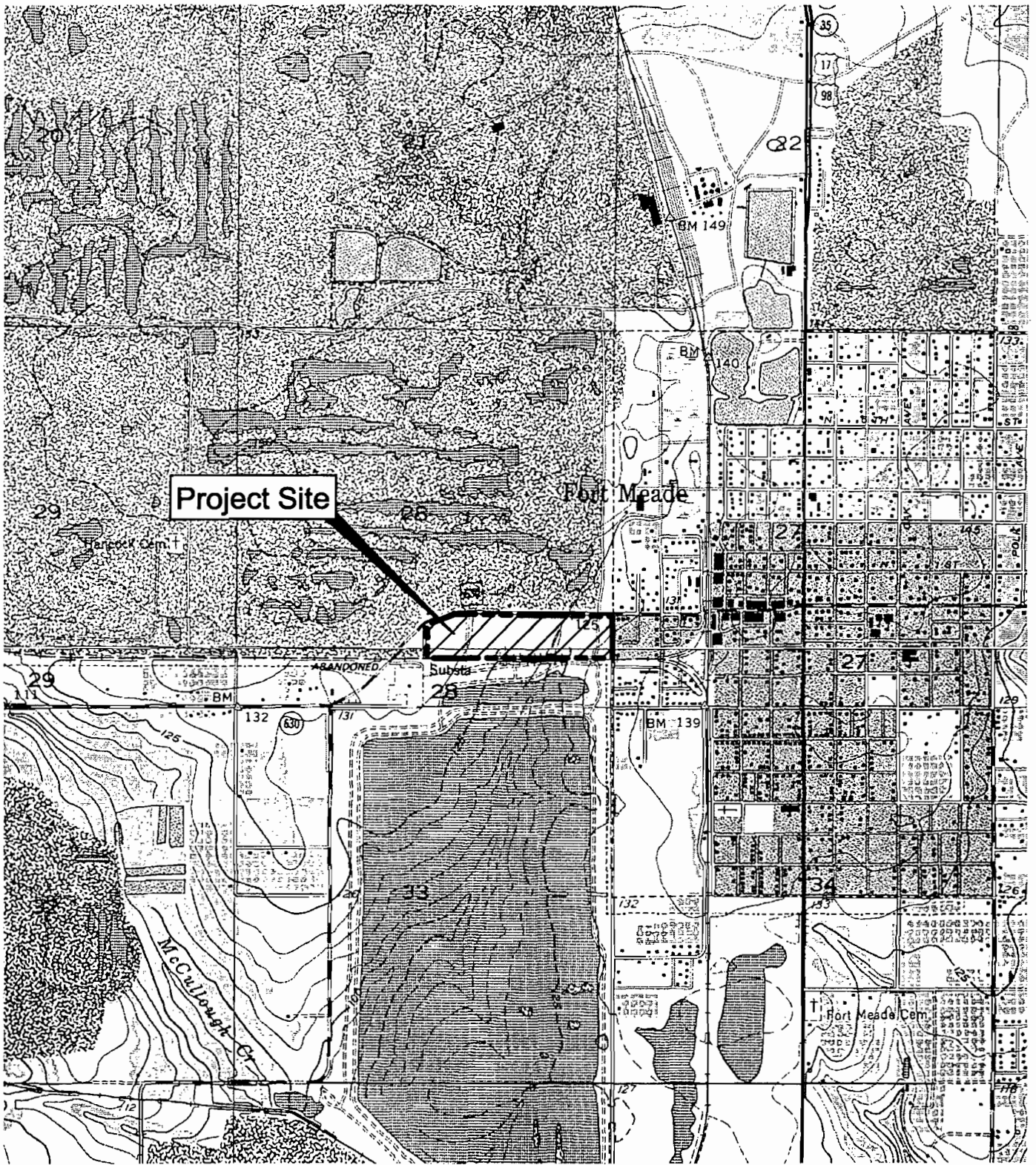
<sup>b</sup> Maximum emission cases:

Operation	Number of Hours for Operation	
	Case A	Case B
Natural gas- 100 % Load	3,390	2,670
Fuel oil- 100 % Load	0	720
Total hours	3,390	3,390



Table 2-4 Maximum Potential Annual Emissions for the Simple Cycle Combustion Turbine Project  
Compared to the PSD Significant Emission Rates

Pollutant	Fuel Load		Annual Emissions (tons/year) based on following hours of operation		Maximum Annual Emissions (tons/year)	PSD Significant Emission Rate (tons/year)	PSD Review Required?
	Gas	100% :	3,390	2,670			
	Oil	100% :	0	720			
SO2			51	152	152	40	Yes
PM			56	68	68	25	Yes
PM10			56	68	68	15	Yes
NOx			352	645	645	40	Yes
CO			174	212	212	100	Yes
VOC (as methane)			21	25	25	40	No
Sulfuric Acid Mist			12	35	35	7	Yes
Mercury			7.29E-06	1.29E-03	1.29E-03	0.1	No
Lead			NEG	7.97E-03	7.97E-03	0.6	No
Fluorides			NEG	2.40E-02	2.40E-02	3	No
MWC Organics (as 2,3,7,8-TCDD)			1.85E-08	2.95E-07	2.95E-07	3.50E-06	No
MWC Metals (as Be and Cd)			NEG	2.63E-03	2.63E-03	15	No
MWC Acid Gases (as HCl)			NEG	1.56E-01	1.56E-01	40	No



REFERENCE

USGS 7.5 Minute Topographic Quadrangles, Homeland & Bowling Green, Florida



Tampa, Florida

Site Location and Topographic Map

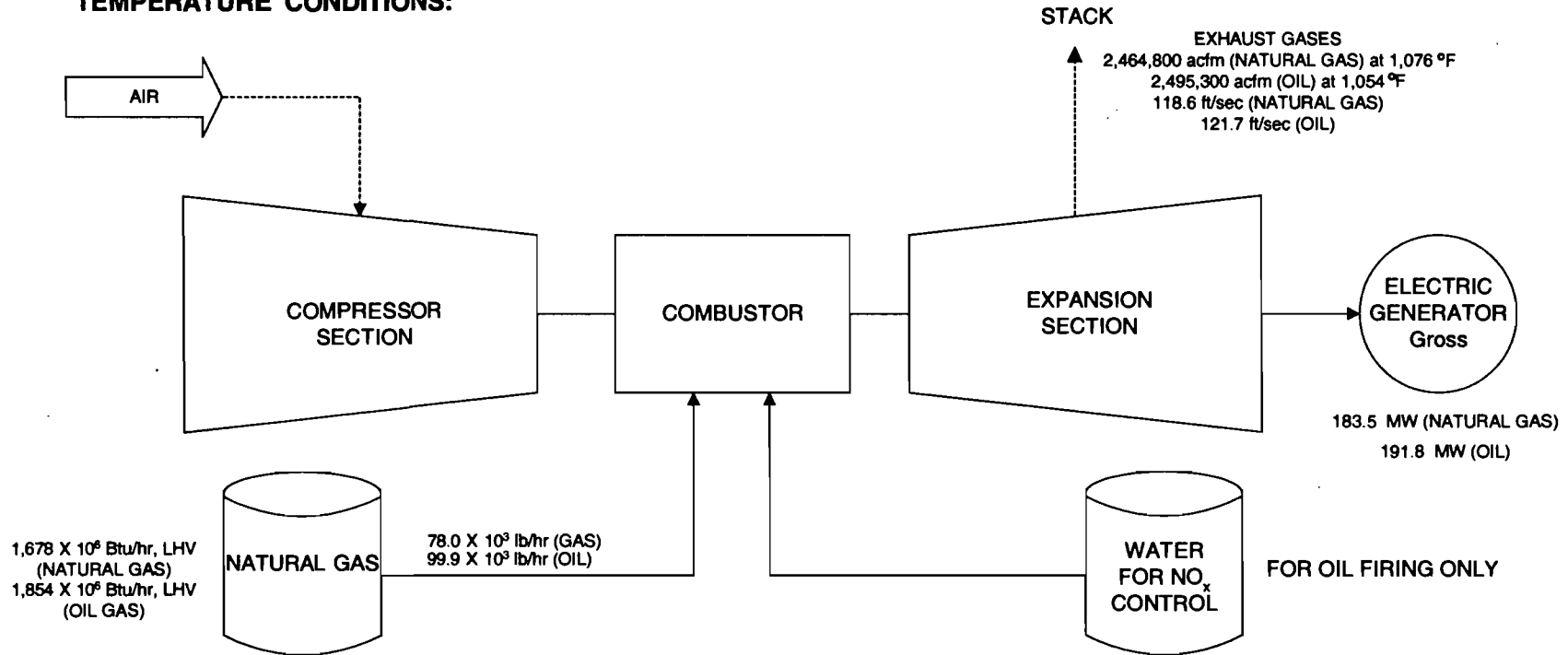
Client / Project

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REV BY:	-	FILE No.:	site-topo.dwg

Job No. 993-9562

FIGURE 2-1

**32°F AMBIENT  
TEMPERATURE CONDITIONS:**



**NOTE: SEE APPENDIX A FOR DESIGN INFORMATION  
AND STACK PARAMETERS FOR EACH FUEL.**

**Figure 2-2**  
Simplified Flow Diagram of Proposed "F" Class  
Combustion Turbine  
Baseload, Winter Design Conditions  
Decker / Peace River Station

Process Flow Legend	
Solid/Liquid	—————>
Gas	- - - - ->
Steam	—————>

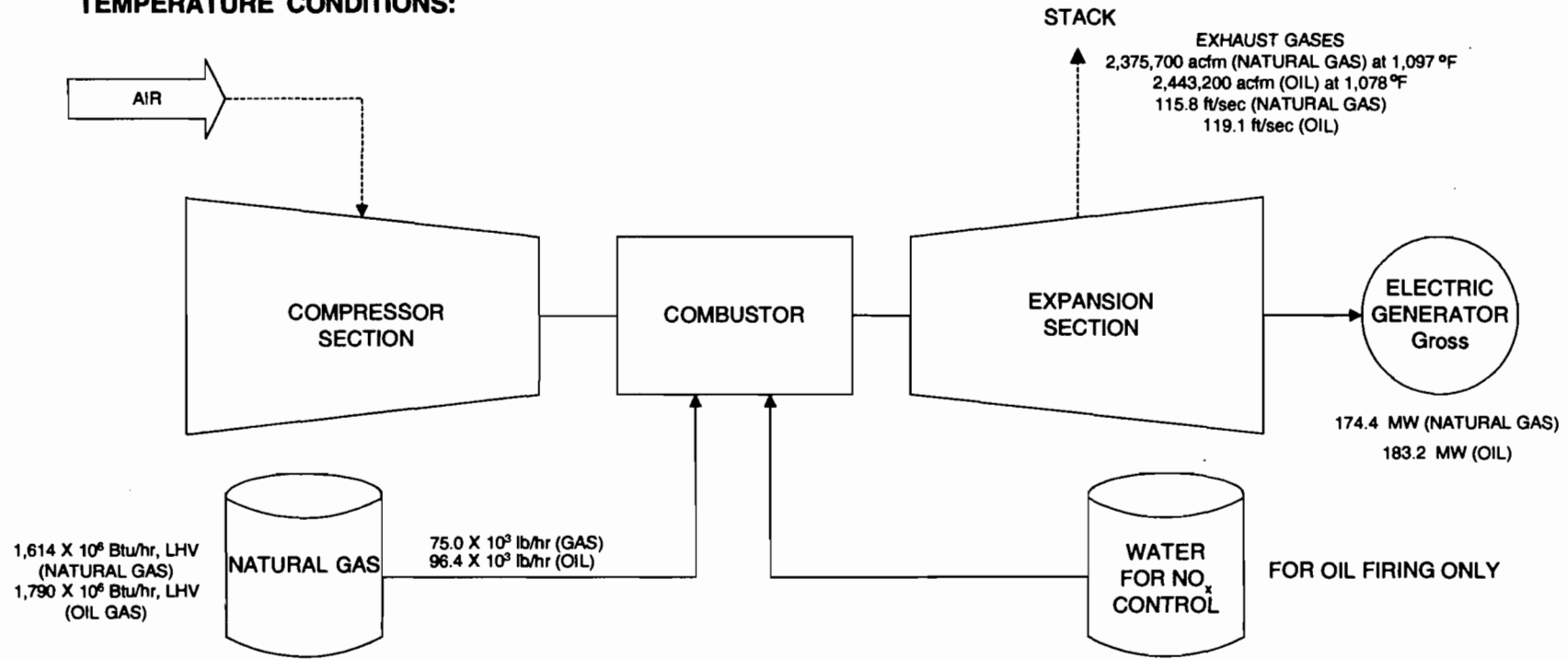
Project No. 9939562-0100

Filename: Peacriver.VSD

Date: 5/17/00



**59°F AMBIENT  
TEMPERATURE CONDITIONS:**



**NOTE:** SEE APPENDIX A FOR DESIGN INFORMATION AND STACK PARAMETERS FOR EACH FUEL.

Figure 2-3  
 Simplified Flow Diagram of Proposed "F" Class  
 Combustion Turbine  
 Baseload, Annual Design Conditions  
 Decker / Peace River Station

**Process Flow Legend**

- Solid/Liquid ———→
- Gas - - - - -→
- Steam ———→

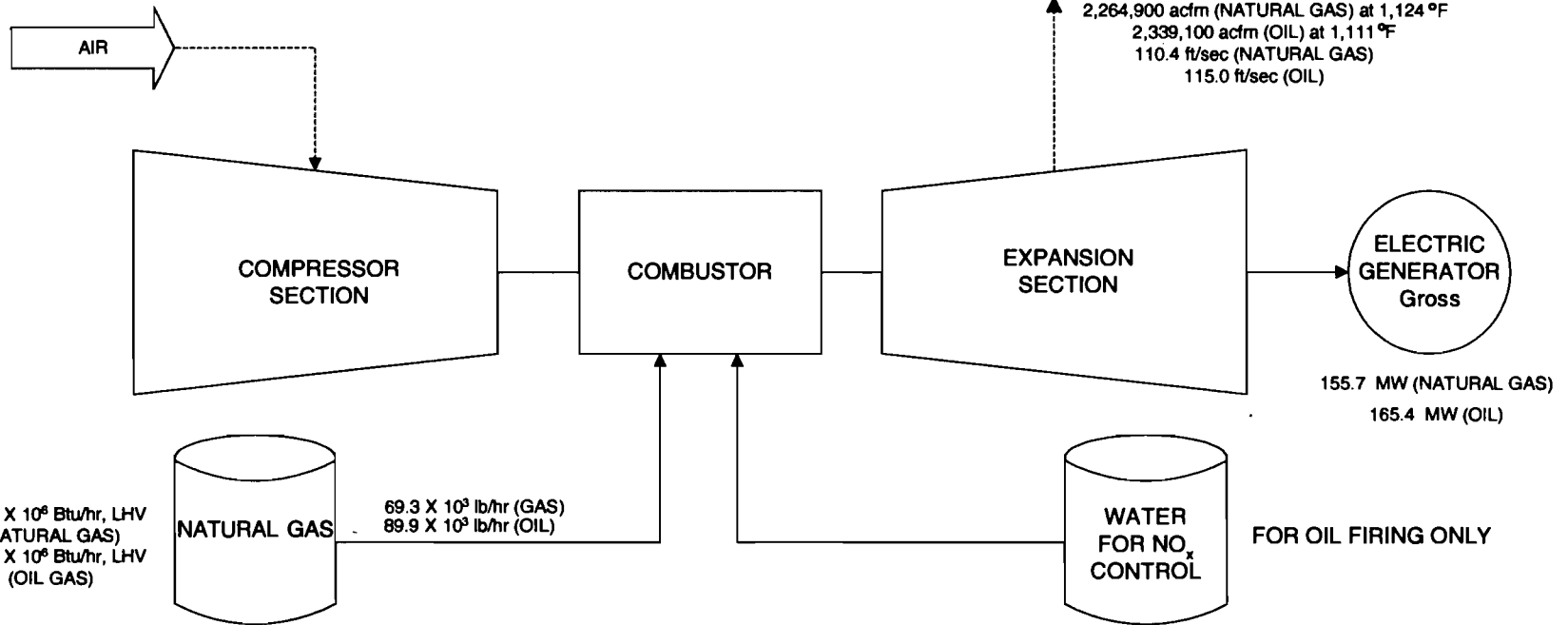
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Filename: Peacriver.VSD

Date: 5/17/00



**95°F AMBIENT  
TEMPERATURE CONDITIONS:**



**NOTE:** SEE APPENDIX A FOR DESIGN INFORMATION AND STACK PARAMETERS FOR EACH FUEL.

2-12

Figure 2-4  
 Simplified Flow Diagram of Proposed "F" Class  
 Combustion Turbine  
 Baseload, Summer Design Conditions  
 Decker / Peace River Station

**Process Flow Legend**

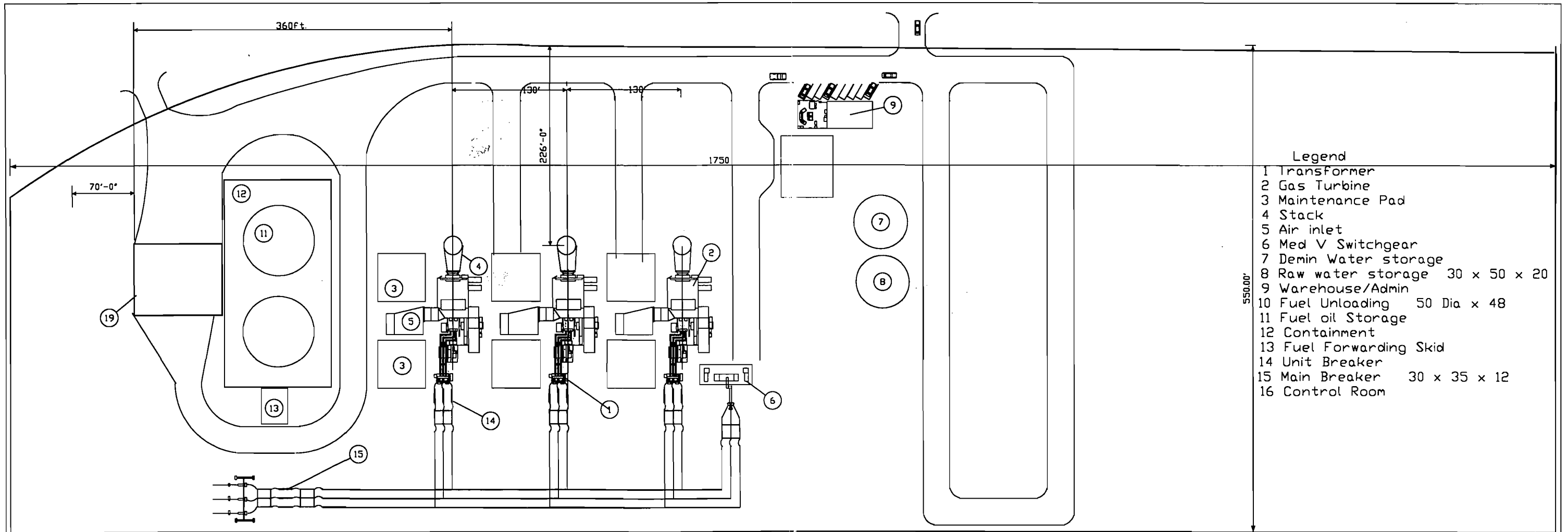
- Solid/Liquid
- Gas
- Steam

Project No. 9939562-0100

Filename: **PeaceRiver.VSD**

Date: 5/17/00





- Legend
- 1 Transformer
  - 2 Gas Turbine
  - 3 Maintenance Pad
  - 4 Stack
  - 5 Air inlet
  - 6 Med V Switchgear
  - 7 Demin Water storage
  - 8 Raw water storage 30 x 50 x 20
  - 9 Warehouse/Admin
  - 10 Fuel Unloading 50 Dia x 48
  - 11 Fuel oil Storage
  - 12 Containment
  - 13 Fuel Forwarding Skid
  - 14 Unit Breaker
  - 15 Main Breaker 30 x 35 x 12
  - 16 Control Room

Peace River Station Fort Meade, Florida			
Nations Energy			
Plant Layout Overlay On Survey	SIZE	FSCM NO	DWG NO
			PRS - 001
	SCALE	1 : 960	SHEET 1 OF 1

### 3.0 AIR QUALITY REVIEW REQUIREMENTS AND APPLICABILITY

The following discussion pertains to the federal and state air regulatory requirements and their applicability to the proposed Peace River Station. These regulations must be satisfied before the proposed Project can begin operation.

#### 3.1 NATIONAL AND STATE AAQS

The existing applicable National and Florida Ambient Air Quality Standards (AAQS) are presented in Table 3-1. National primary AAQS were promulgated to protect the health of the general public, including the young, elderly, and those with respiratory ailments. National secondary AAQS were promulgated to protect the public welfare, including consideration of economic interests, vegetation, visibility, and other factors, with an adequate margin of safety from any known or anticipated adverse effects associated with the presence of pollutants in the ambient air. Areas of the country in violation of AAQS are designated as nonattainment areas, and new sources to be located in or near these areas may be subject to more stringent air permitting requirements.

Florida has adopted EPA's primary and secondary AAQS in Chapter 62-204, F.A.C. In addition, Florida has additional AAQS for SO<sub>2</sub> of 60 and 260 µg/m<sup>3</sup> for the annual and 24-hour averaging periods, respectively, not to be exceeded more than once per year.

#### 3.2 PSD REQUIREMENTS

##### 3.2.1 GENERAL REQUIREMENTS

Under federal and State of Florida PSD review requirements, all major new or modified sources of air pollutants regulated under the Clean Air Act (CAA) must be reviewed and a pre-construction permit issued. Florida's State Implementation Plan (SIP), which contains PSD regulations, has been approved by EPA; therefore, PSD approval authority has been granted to DEP.

A "major facility" is defined as any one of 28 named source categories that have the potential to emit 100 tons per year (TPY) or more or any other stationary facility that has the potential

to emit 250 TPY or more of any pollutant regulated under CAA. "Potential to emit" means the capability, at maximum design capacity, to emit a pollutant after the application of control equipment.

A "major modification" is defined under PSD regulations as a change at an existing major facility that increases emissions by greater than significant amounts. PSD significant emission rates are shown in Table 3-2.

EPA has promulgated as regulations certain increases above an air quality baseline concentration level of SO<sub>2</sub>, PM<sub>10</sub>, and NO<sub>2</sub> concentrations that would constitute significant deterioration. The EPA class designations and allowable PSD increments are presented in Table 3-1. The State of Florida has adopted the EPA class designations and allowable PSD increments for SO<sub>2</sub>, PM<sub>10</sub>, and NO<sub>2</sub> increments.

PSD review is used to determine whether significant air quality deterioration will result from the new or modified facility. Federal PSD requirements are contained in 40 CFR 52.21, Prevention of Significant Deterioration of Air Quality. The State of Florida has adopted PSD regulations by reference [Rule 62-212.400 F.A.C.]. Major facilities and major modifications are required to undergo the following analysis related to PSD for each pollutant emitted in significant amounts:

1. Control technology review,
2. Source impact analysis,
3. Air quality analysis (monitoring),
4. Source information, and
5. Additional impact analyses.

In addition to these analyses, a new facility also must be reviewed with respect to GEP stack height regulations. Discussions concerning each of these requirements are presented in the following sections.



### 3.2.2 CONTROL TECHNOLOGY REVIEW

The control technology review requirements of the federal and state PSD regulations require that all applicable federal and state emission-limiting standards be met, and that BACT be applied to control emissions from the source (Rule 62-212.410, F.A.C.). The BACT requirements are applicable to all regulated pollutants for which the increase in emissions from the facility or modification exceeds the significant emission rate (see Table 3-2).

BACT is defined in 52.21 (b)(12) and Rule 62-210.200(40), F.A.C., as:

An emissions limitation (including a visible emission standard) based on the maximum degree of reduction of each pollutant subject to regulation under the Act which would be emitted by any proposed major stationary source or major modification which the Administrator, on a case-by-case basis, taking into account energy, environmental, and economic impacts, and other costs, determines is achievable through application of production processes and available methods, systems, and techniques (including fuel cleaning or treatment or innovative fuel combustion techniques) for control of such pollutant. In no event shall application of best available control technology result in emissions of any pollutant which would exceed the emissions allowed by any applicable standard under 40 CFR Parts 60 and 61. If the Administrator determines that technological or economic limitations on the application of measurement methodology to a particular part of a source or facility would make the imposition of an emission standard infeasible, a design, equipment, work practice, operational standard or combination thereof, may be prescribed instead to satisfy the requirement for the application of BACT. Such standard shall, to the degree possible, set forth the emissions reductions achievable by implementation of such design, equipment, work practice, or operation and shall provide for compliance by means which achieve equivalent results.

BACT was promulgated within the framework of the PSD requirements in the 1977 amendments of the CAA [Public Law 95-95; Part C, Section 165(a)(4)]. The primary purpose of BACT is to optimize consumption of PSD air quality increments and thereby enlarge the potential for future economic growth without significantly degrading air quality (EPA, 1978; 1980). Guidelines for the evaluation of BACT can be found in EPA's *Guidelines for Determining Best Available Control Technology (BACT)* (EPA, 1978) and in the *PSD Workshop Manual* (EPA, 1980). These guidelines were promulgated by EPA to provide a consistent approach to BACT and to ensure that the impacts of alternative emission control systems are

measured by the same set of parameters. In addition, through implementation of these guidelines, BACT in one area may not be identical to BACT in another area. According to EPA (1980), "BACT analyses for the same types of emissions unit and the same pollutants in different locations or situations may determine that different control strategies should be applied to the different sites, depending on site-specific factors. Therefore, BACT analyses must be conducted on a case-by-case basis."

The BACT requirements are intended to ensure that the control systems incorporated in the design of a proposed facility reflect the latest in control technologies used in a particular industry and take into consideration existing and future air quality in the vicinity of the proposed facility. BACT must, as a minimum, demonstrate compliance with new source performance standards (NSPS) for a source (if applicable). An evaluation of the air pollution control techniques and systems, including a cost-benefit analysis of alternative control technologies capable of achieving a higher degree of emission reduction than the proposed control technology, is required. The cost-benefit analysis requires the documentation of the materials, energy, and economic penalties associated with the proposed and alternative control systems, as well as the environmental benefits derived from these systems. A decision on BACT is to be based on sound judgment, balancing environmental benefits with energy, economic, and other impacts (EPA, 1978).

Historically, a "bottom-up" approach consistent with the BACT Guidelines and PSD Workshop Manual has been used. With this approach, an initial control level, which is usually NSPS, is evaluated against successively more stringent controls until a BACT level is selected. However, EPA developed a concern that the bottom-up approach was not providing the level of BACT decisions originally intended. As a result, in December 1987, the EPA Assistant Administrator for Air and Radiation mandated changes in the implementation of the PSD program, including the adoption of a new "top-down" approach to BACT decision making.

The top-down BACT approach essentially starts with the most stringent (or top) technology and emissions limit that have been applied elsewhere to the same or a similar source category. The applicant must next provide a basis for rejecting this technology in favor of the next most stringent technology or propose to use it. Rejection of control alternatives may be based on technical or economic infeasibility. Such decisions are made on the basis of physical differences (e.g., fuel type), location differences (e.g., availability of water), or significant differences that may exist in the environmental, economic, or energy impacts. The differences between the proposed facility and the facility on which the control technique was applied previously must be justified. EPA has issued a draft guidance document on the top-down approach entitled *Top-Down Best Available Control Technology Guidance Document* (EPA, 1990).

### 3.2.3 SOURCE IMPACT ANALYSIS

A source impact analysis must be performed for a proposed major source subject to PSD review for each pollutant for which the increase in emissions exceeds the significant emission rate (Table 3-2). The PSD regulations specifically provide for the use of atmospheric dispersion models in performing impact analyses, estimating baseline and future air quality levels, and determining compliance with AAQS and allowable PSD increments. Designated EPA models normally must be used in performing the impact analysis. Specific applications for other than EPA-approved models require EPA's consultation and prior approval. Guidance for the use and application of dispersion models is presented in the EPA publication *Guideline on Air Quality Models (Revised)*. The source impact analysis for criteria pollutants to address compliance with AAQS and PSD Class II increments may be limited to the new or modified source if the net increase in impacts as a result of the new or modified source is above significance levels, as presented in Table 3-1.

The EPA has proposed significant impact levels (SILs) for Class I areas. The National Park Service (NPS) as the designated agency for oversight in air quality impacts to Class I areas has also recommended significant impact levels for PSD Class I areas. The EPA proposed Class I SILs are as follows:

Pollutant	Averaging Time	Proposed EPA PSD Class I Significant Impact Levels ( $\mu\text{g}/\text{m}^3$ )
SO <sub>2</sub>	3-hour	1
	24-hour	0.2
	Annual	0.1
PM <sub>10</sub>	24-hour	0.3
	Annual	0.2
NO <sub>2</sub>	Annual	0.1

<sup>a</sup>  $\mu\text{g}/\text{m}^3$  = micrograms per cubic meter.

Although these levels have not been officially promulgated as part of the PSD review process and may not be binding for states in performing PSD review, the proposed levels serve as a guideline in assessing a source's impact in a Class I area. The EPA action to incorporate Class I significant impact levels in the PSD process is part of implementing NSR provisions of the 1990 CAA Amendments. Because the process of developing the regulations will be lengthy, EPA believes that the proposed rules concerning the significant impact levels is appropriate in order to assist states in implementing the PSD permit process.

Various lengths of record for meteorological data can be used for impact analysis. A 5-year period can be used with corresponding evaluation of highest, second-highest short-term concentrations for comparison to AAQS or PSD increments. The term "highest, second-highest" (HSH) refers to the highest of the second-highest concentrations at all receptors (i.e., the highest concentration at each receptor is discarded). The second-highest concentration is significant because short-term AAQS specify that the standard should not be exceeded at any location more than once a year. If fewer than 5 years of meteorological data are used in the modeling analysis, the highest concentration at each receptor normally must be used for comparison to air quality standards.

The term "baseline concentration" evolves from federal and state PSD regulations and refers to a concentration level corresponding to a specified baseline date and certain additional baseline sources. By definition, in the PSD regulations as amended August 7, 1980, baseline

concentration means the ambient concentration level that exists in the baseline area at the time of the applicable baseline date. A baseline concentration is determined for each pollutant for which a baseline date is established and includes:

1. The actual emissions representative of facilities in existence on the applicable baseline date; and
2. The allowable emissions of major stationary facilities that commenced construction before January 6, 1975, for SO<sub>2</sub> and PM(TSP) concentrations, or February 8, 1988, for NO<sub>2</sub> concentrations, but that were not in operation by the applicable baseline date.

The following emissions are not included in the baseline concentration and therefore affect PSD increment consumption:

1. Actual emissions from any major stationary facility on which construction commenced after January 6, 1975, for SO<sub>2</sub> and PM(TSP) concentrations, and after February 8, 1988, for NO<sub>2</sub> concentrations; and
2. Actual emission increases and decreases at any stationary facility occurring after the baseline date.

In reference to the baseline concentration, the term "baseline date" actually includes three different dates:

1. The major facility baseline date, which is January 6, 1975, in the cases of SO<sub>2</sub> and PM(TSP), and February 8, 1988, in the case of NO<sub>2</sub>.
2. The minor facility baseline date, which is the earliest date after the trigger date on which a major stationary facility or major modification subject to PSD regulations submits a complete PSD application.
3. The trigger date, which is August 7, 1977, for SO<sub>2</sub> and PM(TSP), and February 8, 1988, for NO<sub>2</sub>.

The minor source baseline date for SO<sub>2</sub> and PM(TSP) has been set as December 27, 1977, for the entire State of Florida (Rule 62-275.700(1)(a), F.A.C.). The minor source baseline for NO<sub>2</sub>

has been set as March 28, 1988 (Rule 62-275.700(3)(a), F.A.C). It should be noted that references to PM (TSP) are also applicable to PM<sub>10</sub>.

#### **3.2.4 AIR QUALITY MONITORING REQUIREMENTS**

In accordance with requirements of 40 CFR 52.21(m) and Rule 62-212.400(5)(f), F.A.C., any application for a PSD permit must contain an analysis of continuous ambient air quality data in the area affected by the proposed major stationary facility or major modification. For a new major facility, the affected pollutants are those that the facility potentially would emit in significant amounts. For a major modification, the pollutants are those for which the net emissions increase exceeds the significant emission rate (see Table 3-2).

Ambient air monitoring for a period of up to 1 year generally is appropriate to satisfy the PSD monitoring requirements. A minimum of 4 months of data is required. Existing data from the vicinity of the proposed source may be used if the data meet certain quality assurance requirements; otherwise, additional data may need to be gathered. Guidance in designing a PSD monitoring network is provided in EPA's *Ambient Monitoring Guidelines for Prevention of Significant Deterioration* (EPA, 1987a).

The regulations include an exemption that excludes or limits the pollutants for which an air quality analysis must be conducted. This exemption states that Florida DEP may exempt a proposed major stationary facility or major modification from the monitoring requirements with respect to a particular pollutant if the emissions increase of the pollutant from the facility or modification would cause, in any area, air quality impacts less than the *de minimis* levels presented in Table 3-2 (Rule 62-212.400-3, F.A.C.).

#### **3.2.5 SOURCE INFORMATION/GOOD ENGINEERING PRACTICE STACK HEIGHT**

Source information must be provided to adequately describe the proposed Project. The general type of information required for this Project is presented in Section 2.0.

The 1977 CAA Amendments require that the degree of emission limitation required for control of any pollutant not be affected by a stack height that exceeds GEP or any other dispersion technique. On July 8, 1985, EPA promulgated final stack height regulations (EPA, 1985a). Identical regulations have been adopted by Florida DEP (Rule 62-210.550, F.A.C.).

GEP stack height is defined as the highest of:

1. 65 meters (m); or
2. A height established by applying the formula:  
$$H_g = H + 1.5L$$
where:  $H_g$  = GEP stack height,  
 $H$  = Height of the structure or nearby structure, and  
 $L$  = Lesser dimension (height or projected width) of nearby structure(s); or
3. A height demonstrated by a fluid model or field study.

"Nearby" is defined as a distance up to five times the lesser of the height or width dimensions of a structure or terrain feature, but not greater than 0.8 km. Although GEP stack height regulations require that the stack height used in modeling for determining compliance with AAQS and PSD increments not exceed the GEP stack height, the actual stack height may be greater.

The stack height regulations also allow increased GEP stack height beyond that resulting from the above formula in cases where plume impaction occurs. Plume impaction is defined as concentrations measured or predicted to occur when the plume interacts with elevated terrain. Elevated terrain is defined as terrain that exceeds the height calculated by the GEP stack height formula.

### 3.2.6 ADDITIONAL IMPACT ANALYSIS

In addition to air quality impact analyses, federal and State of Florida PSD regulations require analyses of the impairment to visibility and the impacts on soils and vegetation that would occur as a result of the proposed source [40 CFR 52.21(o); Rule 62-212.400(5)(e),

F.A.C.]. These analyses are to be conducted primarily for PSD Class I areas. Impacts as a result of general commercial, residential, industrial, and other growth associated with the source also must be addressed. These analyses are required for each pollutant emitted in significant amounts (Table 3-2).

### **3.3 NONATTAINMENT RULES**

Based on the current nonattainment provisions (Rule 62-212.500, F.A.C.), all major new facilities and modifications to existing major facilities located in a nonattainment area must undergo nonattainment review. A new major facility is required to undergo this review if the proposed pieces of equipment have the potential to emit 100 TPY or more of the nonattainment pollutant. A major modification at a major facility is required to undergo review if it results in a significant net emission increase of 40 TPY or more of the nonattainment pollutant or if the modification is major (i.e., 100 TPY or more).

For major facilities or major modifications that locate in an attainment or unclassifiable area, the nonattainment review procedures apply if the source or modification is located within the area of influence of a nonattainment area. The area of influence is defined as an area that is outside the boundary of a nonattainment area but within the locus of all points that are 50 km outside the boundary of the nonattainment area. Based on Rule 62-2.500(2)(c)2.a., F.A.C., all VOC sources that are located within an area of influence are exempt from the provisions of NSR for nonattainment areas. Sources that emit other nonattainment pollutants and are located within the area of influence are subject to nonattainment review unless the maximum allowable emissions from the proposed source do not have a significant impact within the nonattainment area.

### **3.4 EMISSION STANDARDS**

#### **3.4.1 NEW SOURCE PERFORMANCE STANDARDS**

The NSPS are a set of national emission standards that apply to specific categories of new sources. As stated in the CAA Amendments of 1977, these standards "shall reflect the degree of emission limitation and the percentage reduction achievable through application of the



best technological system of continuous emission reduction the Administrator determines has been adequately demonstrated."

The proposed Project will be subject to one or more NSPS. The CTs will be subject to 40 CFR Part 60, Subpart GG, and each fuel oil storage tank (2.8 million gallon capacity) will be subject to 40 CFR Part 60, Subpart Kb.

#### **3.4.1.1 Combustion Turbine**

The CTs will be subject to emission limitations covered under Subpart GG, which limits NO<sub>x</sub> and SO<sub>2</sub> emissions from all stationary combustion turbines with a heat input at peak load equal to 10.7 gigajoules per hour (10 mmBtu/hr), based on the lower heating value of the fuel fired.

NO<sub>x</sub> emissions are limited to 75 ppmvd corrected to 15 percent oxygen and heat rate while sulfur dioxide emissions are limited to using a fuel with a sulfur content of 0.8 percent. In addition to emission limitations, there are requirements for notification, record keeping, reporting, performance testing and monitoring. These are summarized below:

##### **40 CFR 60.7 Notification and Record Keeping**

- (a)(1) Notification of the date of construction - 30 days after such date.
- (a)(2) Notification of the date of initial start-up - no more than 60 days or less than 30 days prior to date.
- (a)(3) Notification of actual date of initial start-up - within 15 days after such date.
- (a)(5) Notification of date which demonstrates CEM - not less than 30 days prior to date.

60.7 (b) Maintain records of the start-up, shutdown, and malfunction quarterly.

- (c) Excess emissions reports - by the 30th day following end of quarter. (required even if no excess emissions occur)

- (d) Maintain file of all measurements for two years.

#### 60.8 Performance Tests

- (a) must be performed within 60 days after achieving maximum production rate but no later than 180 days after initial start-up.
- (d) Notification of Performance tests at least 30 days prior to them occurring.

#### 40 CFR Subpart GG

##### 60.334 Monitoring of Operations

- (a) continuous monitoring system required for water-to-fuel ratio to meet NSPS; system must be accurate within  $\pm 5$  percent.
- (b) Monitor sulfur and nitrogen content of fuel.
  - Oil - (1): each occasion that fuel is transferred to bulk storage tank.
  - Gas - (2): daily monitoring required

#### 3.4.1.2 Fuel Oil Storage Tank

The applicable NSPS is 40 CFR Part 60, Subpart Kb--Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels for which Construction, Reconstruction, or Modification Commenced after July 23, 1984). The storage tank will contain distillate fuel oil, a volatile organic liquid as defined in Subpart Kb. There are no emission limiting or control requirements under Subpart Kb for the use of distillate fuel oil. The facility, however, must perform record keeping of the type of organic liquid in the tank.

#### 3.4.2 FLORIDA RULES

The Florida DEP regulations for new stationary sources are covered in the F.A.C. The Florida DEP has adopted the EPA NSPS by reference in Rule 62-204.800(7); subsection (b)38 for stationary gas turbines and (b)15 for volatile organic liquid storage vessels. Therefore, the Project is required to meet the same emissions, performance testings, monitoring,

reporting, and record keeping as those described in Section 3.4.1. DEP has authority for implementing NSPS requirements in Florida.

### **3.4.3 FLORIDA AIR PERMITTING REQUIREMENTS**

The Florida DEP regulations require any new source to obtain an air permit prior to construction. Major new sources must meet the appropriate PSD and nonattainment requirements as discussed previously. Required permits and approvals for air pollution sources include NSR for nonattainment areas, PSD, NSPS, National Emission Standards for Hazardous Air Pollutants (NESHAP), Permit to Construct, and Permit to Operate. The requirements for construction permits and approvals are contained in Rules 62-4.030, 62-4.050, 62-4.052, 62-4.210, and 62-210.300(1), F.A.C. Specific emission standards are set forth in Chapter 62-296, F.A.C.

### **3.4.4 HAZARDOUS POLLUTANT REVIEW**

The Florida DEP has published guidelines (DEP, 1995) to determine whether any emission of a potentially hazardous or toxic pollutant can pose a possible health risk to the public. Maximum concentrations for all regulated pollutants for which an ambient standard does not exist and all nonregulated hazardous pollutants can be compared to ambient reference concentrations (ARCs) for each applicable pollutant. If the maximum predicted concentrations for any hazardous pollutant is less than the corresponding ARC for each applicable averaging time, that emission is considered not to pose a significant health risk. The ARCs are not environmental standards but, rather, evaluation tools to determine if an apparent threat to the public health may exist. These levels are not used in permitting new sources.

### **3.4.5 LOCAL AIR REGULATIONS**

Polk County does not have more stringent air regulations than those promulgated by the DEP.

### **3.5 SOURCE APPLICABILITY**

#### **3.5.1 AREA CLASSIFICATION**

The Project site is located in Polk County, which has been designated by EPA and DEP as an attainment area for all criteria pollutants. Polk County and surrounding counties are designated as PSD Class II areas for SO<sub>2</sub>, PM<sub>10</sub>, and NO<sub>2</sub>. The nearest Class I area to the site is the Chassahowitzka National Wilderness Area (NWA) which is about 124 km (74 miles) from the site.

#### **3.5.2 PSD REVIEW**

##### **3.5.2.1 Pollutant Applicability**

The Project is considered to be a major facility because the emissions for one regulated pollutant is estimated to exceed 250 TPY; therefore, PSD review is required for any pollutant for which the emissions are considered major or exceed the PSD significant emission rates. As shown in Table 3-3, potential emissions from the proposed Project will be major for NO<sub>x</sub> and greater than the significant emission rates for PM (TSP), PM<sub>10</sub>, SO<sub>2</sub>, CO, and sulfuric acid mist. Because the proposed Project impacts for these pollutants are predicted to be below the significant impact levels, a modeling analysis incorporating the impacts from other sources is not required. (Note: EPA has promulgated changes to the PSD Rules to eliminate hazardous air pollutants (HAPs) from PSD review. The pollutants, vinyl chloride, mercury, asbestos, and beryllium, are no longer evaluated in PSD review.)

As part of the PSD review, a PSD Class I increment analysis is required if the proposed Project's impacts are greater than the proposed EPA Class I significant impact levels. Because the nearest Class I areas to the plant site is about 124 km from the site, a PSD Class I increment-consumption analysis is required.

##### **3.5.2.2 Emission Standards**

The applicable NSPS for the CTs is 40 CFR Part 60, Subpart GG. The proposed emissions for the turbines will be well below the specified limits (see Section 4.0). The fuel oil storage tanks will each have a nominal storage capacity of 1.5 million gallons of distillate fuel oil.

Since each storage tank has a capacity greater than 40 cubic meters (m<sup>3</sup>) [approximately gallons], the applicable NSPS is 40 CFR Part 60, Subpart Kb. Each storage tank will contain distillate fuel oil, a volatile organic liquid as defined in Subpart Kb, with a true vapor pressure of 0.022 pound per square inch (psi) at 100 F. Because the fuel oil is expected to have a maximum true vapor pressure of less than 3.5 kilopascals (kPa) or 0.51 psi, only the minor monitoring of operating requirements specified in 40 CFR 60 116b(a) and (b) will apply.

### 3.5.2.3 Ambient Monitoring

Based on the estimated pollutant emissions from the proposed plant (see Table 3-4), a pre-construction ambient monitoring analysis is required for PM<sub>10</sub>, SO<sub>2</sub>, NO<sub>2</sub>, CO, and sulfuric acid mist. If the net increase in impact of other pollutants is less than the applicable *de minimis* monitoring concentration, then an exemption from the pre-construction ambient monitoring requirement is authorized by Rule 62-212.400(3)(e) F.A.C. In addition, if an acceptable ambient monitoring method for the pollutant has not been established by EPA, monitoring is not required.

If pre-construction monitoring data are required to be submitted, data collected at or near the Project site can be submitted, based on existing air quality data or the collection of onsite data.

Pre-construction monitoring data should not be required to be submitted for the Project because, as shown in Table 3-4, impacts are predicted to be below the applicable *de minimis* monitoring concentration (see Table 3-2) for all pollutants. For sulfuric acid mist, although the Project's emissions are greater than the significant emission rate, EPA has established no acceptable monitoring method for this pollutant. Therefore, an exemption from the preconstruction monitoring requirement for sulfuric acid is requested in accordance with the PSD regulations.

#### **3.5.2.4 GEP Stack Height Analysis**

The GEP stack height regulations allow any stack to be at least 65 m [213 feet (ft)] high. The CT stacks for the Project will be 60 ft. This stack height does not exceed the GEP stack height. However, as discussed in Section 6.0, Air Quality Modeling Approach, since the stack height is less than GEP, building downwash effects must be considered in the modeling analysis. As a result, the potential for downwash of the CTs' emissions caused by nearby structures are included in the modeling analysis.

#### **3.5.3 NONATTAINMENT REVIEW**

The Project site is located in Polk County, which is classified as an attainment area for all criteria pollutants. Therefore, nonattainment requirements are not applicable.

#### **3.5.4 OTHER CLEAN AIR ACT REQUIREMENTS**

The 1990 CAA Amendments established a program to reduce potential precursors of acidic deposition. The Acid Rain Program was delineated in Title IV of the CAA Amendments and required EPA to develop the program. EPA's final regulations were promulgated on January 11, 1993, and included permit provisions (40 CFR Part 72), allowance system (Part 73), continuous emission monitoring (Part 75), excess emission procedures (Part 77), and appeal procedures (Part 78).

EPA's Acid Rain Program applies to all existing and new utility units except those serving a generator less than 25 MW, existing simple cycle CTs, and certain non-utility facilities; units which fall under the program are referred to as affected units. The EPA regulations would be applicable to the proposed Project for the purposes for obtaining a permit and allowances, as well as emission monitoring. New units are required to obtain permits under the program by submitting a complete application 24 months before the later of January 1, 2000, or the date on which the unit begins serving an electric generator (greater than 25 MW).

The permit would provide SO<sub>2</sub> and NO<sub>x</sub> emission limitations and the requirement to hold emission allowances. Emission limitations established in the Acid Rain Program are presumed to be less stringent than BACT or lowest achievable emission rate (LAER) for new units. An allowance is a market-based financial instrument that is equivalent to 1 ton of SO<sub>2</sub> emissions. Allowances can be sold, purchased, or traded. For the proposed Project, SO<sub>2</sub> allowances will be obtained from the market.

Continuous emission monitoring (CEM) for SO<sub>2</sub> and NO<sub>x</sub> is required for gas-fired and oil-fired affected units. When an SO<sub>2</sub> CEM is selected to monitor SO<sub>2</sub> mass emissions, a flow monitor is also required. Alternately, SO<sub>2</sub> emissions may be determined using procedures established in Appendix D, 40 CFR Part 75 (flow proportional oil sampling or manual daily oil sampling). CO<sub>2</sub> emissions must also be determined either through a CEM (e.g., as a diluent for NO<sub>x</sub> monitoring) or calculation. Alternate procedures, test methods, and quality assurance/quality control (QA/QC) procedures for CEM are specified (Part 75 Appendices A through I). The CEM requirements including QA/QC procedures are, in general, more stringent than those specified in the NSPS for Subpart GG. New units are required to meet the requirements by the later of January 1, 1995, or not later than 90 days after the unit commences commercial operation.

The EPA has, and is currently developing, emissions standards for HAPs for various industrial categories. These new National Emission Standards for Hazardous Air Pollutants (NESHAPs) that result from the 1990 CAA Amendments are based on the use of Maximum Achievable Control Technology (MACT). The adopted standards are contained in 40 CFR 63. New sources that emit more than 10 TPY of a single HAP or 25 TPY of total HAPs are required to apply MACT for the promulgated industrial category or to obtain a case-by-case MACT determination from the applicable regulatory authority after submitting a MACT analysis. EPA is currently developing NESHAP for stationary combustion turbines. The proposed NESHAP are anticipated in late 2000 with promulgation in early 2002. For the Project, emissions of HAPs will be less than 10 TPY of a single HAP and 25 TPY of all HAPs.

Table 3-1. National and State AAQS, Allowable PSD Increments, and Significant Impact Levels

Pollutant	Averaging Time	AAQS ( $\mu\text{g}/\text{m}^3$ )			PSD Increments ( $\mu\text{g}/\text{m}^3$ )		Significant Impact Levels ( $\mu\text{g}/\text{m}^3$ ) <sup>b</sup>
		Primary Standard	Secondary Standard	Florida	Class I	Class II	
Particulate Matter <sup>f</sup> (PM <sub>10</sub> )	Annual Arithmetic Mean	50	50	50	4	17	1
	24-Hour Maximum	150	150	150	8	30	5
Sulfur Dioxide	Annual Arithmetic Mean	80	NA	60	2	20	1
	24-Hour Maximum	365	NA	260	5	91	5
	3-Hour Maximum	NA	1,300	1,300	25	512	25
Carbon Monoxide	8-Hour Maximum	10,000	10,000	10,000	NA	NA	500
	1-Hour Maximum	40,000	40,000	40,000	NA	NA	2,000
Nitrogen Dioxide	Annual Arithmetic Mean	100	100	100	2.5	25	1
Ozone <sup>c</sup>	8-Hour Maximum <sup>d</sup>	157	157	157	NA	NA	NA
Lead	Calendar Quarter Arithmetic Mean	1.5	1.5	1.5	NA	NA	NA

Note: Particulate matter (PM<sub>10</sub>) = particulate matter with aerodynamic diameter less than or equal to 10 micrometers.

NA = Not applicable, i.e., no standard exists.

<sup>a</sup> Short-term maximum concentrations are not to be exceeded more than once per year.

<sup>b</sup> Maximum concentrations are not to be exceeded.

<sup>c</sup> On July 18, 1997, EPA promulgated revised AAQS for particulate matter and ozone. For particulate matter, PM<sub>2.5</sub> standards were introduced with a 24-hour standard of 65  $\mu\text{g}/\text{m}^3$  (3-year average of 98<sup>th</sup> percentile) and an annual standard of 15  $\mu\text{g}/\text{m}^3$  (3-year average at community monitors). These standards have been stayed by a court case against EPA and implementation of these standards are many years away pending EPA appeal.

<sup>d</sup> 0.08 ppm; achieved when 3-year average of 99<sup>th</sup> percentile is 0.08 ppm or less. These have been stayed by a court case against EPA. EPA is appealing. The 1-hour standard of 0.12 ppm is still applicable. FDEP has not yet adopted the new standards.

Sources: Federal Register, Vol. 43, No. 118, June 19, 1978.

40 CFR 50; 40 CFR 52.21.

Chapter 62-272, F.A.C.



Table 3-2. PSD Significant Emission Rates and *De Minimis* Monitoring Concentrations

Pollutant	Regulated Under	Significant Emission Rate (TPY)	<i>De Minimis</i> Monitoring Concentration <sup>a</sup> (µg/m <sup>3</sup> )
Sulfur Dioxide	NAAQS, NSPS	40	13, 24-hour
Particulate Matter [PM(TSP)]	NSPS	25	10, 24-hour
Particulate Matter (PM <sub>10</sub> )	NAAQS	15	10, 24-hour
Nitrogen Dioxide	NAAQS, NSPS	40	14, annual
Carbon Monoxide	NAAQS, NSPS	100	575, 8-hour
Volatile Organic Compounds (Ozone)	NAAQS, NSPS	40	100 TPY <sup>b</sup>
Lead	NAAQS	0.6	0.1, 3-month
Sulfuric Acid Mist	NSPS	7	NM
Total Fluorides	NSPS	3	0.25, 24-hour
Total Reduced Sulfur	NSPS	10	10, 1-hour
Reduced Sulfur Compounds	NSPS	10	10, 1-hour
Hydrogen Sulfide	NSPS	10	0.2, 1-hour
Mercury	NESHAP	0.1	0.25, 24-hour
MWC Organics	NSPS	3.5x10 <sup>-6</sup>	NM
MWC Metals	NSPS	15	NM
MWC Acid Gases	NSPS	40	NM
MSW Landfill Gases	NSPS	50	NM

Note: Ambient monitoring requirements for any pollutant may be exempted if the impact of the increase in emissions is below *de minimis* monitoring concentrations.

NAAQS = National Ambient Air Quality Standards.

NM = No ambient measurement method established; therefore, no *de minimis* concentration has been established.

NSPS = New Source Performance Standards.

NESHAP = National Emission Standards for Hazardous Air Pollutants.

g/m<sup>3</sup> = micrograms per cubic meter.

MWC = Municipal waste combustor

MSW = Municipal solid waste

<sup>a</sup> Short-term concentrations are not to be exceeded.

<sup>b</sup> No *de minimis* concentration; an increase in VOC emissions of 100 TPY or more will require monitoring analysis for ozone.

<sup>c</sup> Any emission rate of these pollutants.

Sources: 40 CFR 52.21.  
Rule 62-212.400

Table 3-3. Maximum Emissions Due to the Proposed Peace River Station Compared to the PSD Significant Emission Rates

Pollutant	Pollutant Emissions (TPY)		PSD Review
	Potential Emissions from Proposed Facility <sup>a</sup>	Significant Emission Rate	
Sulfur Dioxide	152	40	Yes
Particulate Matter [PM(TSP)]	68	25	Yes
Particulate Matter (PM <sub>10</sub> )	68	15	Yes
Nitrogen Dioxide	645	40	Yes
Carbon Monoxide	212	100	Yes
Volatile Organic Compounds	25	40	No
Sulfuric Acid Mist	35	7	Yes
Mercury	1.29E-03	0.1	<del>Yes</del>
Lead	7.97E-03	0.6	No
Total Fluorides	2.40E-02	3	No
Total Reduced Sulfur	NEG	10	No
Reduced Sulfur Compounds	NEG	10	No
Hydrogen Sulfide	NEG	10	No
MWC Organics (as 2,3,7,8-TCDD)	2.95E-07	3.5x10 <sup>-6</sup>	No
MWC Metals (as Be, Cd)	2.63E-03	15	No
MWC Acid Gaser (as HCl)	1.56E-01	40	No

Note: NEG = Negligible.

- <sup>a</sup> Based on emissions from operating at baseload at 59°F; firing natural gas and distillate fuel oil for 2,670 and 720 hours per year per turbine for a total of three CTs, respectively (Refer to Table 2-4).

Table 3-4. Predicted Net Increase in Impacts Due to the Proposed Peace River Station Compared to PSD *De Minimis* Monitoring Concentrations

Pollutant	Concentration ( $\mu\text{g}/\text{m}^3$ )	
	Predicted Increase in Impacts <sup>a</sup>	<i>De Minimis</i> Monitoring Concentration
Sulfur Dioxide	0.96	13, 24-hour
Particulate Matter (PM <sub>10</sub> )	0.28	10, 24-hour
Nitrogen Dioxide	0.23	14, annual
Carbon Monoxide	1.4	575, 8-hour

Note: NA = not applicable.

NM = no ambient measurement method.

TPY = tons per year.

<sup>a</sup> See Section 6.0 for air dispersion modeling results. These results are based on firing fuel oil and are higher than those for firing natural gas.

## 4.0 CONTROL TECHNOLOGY REVIEW

### 4.1 APPLICABILITY

The PSD regulations require new major stationary sources to undergo a control technology review for each pollutant that may potentially be emitted above significant amounts. The control technology review requirements of the PSD regulations are applicable to emissions of NO<sub>x</sub>, SO<sub>2</sub>, CO, and PM/PM<sub>10</sub> (see Section 3.0). The maximum potential annual emissions of these pollutants from the proposed GE 7FA CTs are summarized below (see Table 2-7):

Pollutant Emissions (TPY)	
Pollutant	3 GE 7FA CTs
NO <sub>x</sub>	644.7
SO <sub>2</sub>	151.5
CO	212.4
PM/PM <sub>10</sub>	67.8

<sup>a</sup> Maximum emissions based on firing natural gas for 2,670 hours and distillate fuel oil for 720 hours at baseload conditions and 59°F.

This section presents the applicable NSPS and the proposed BACT for these pollutants. The approach to the BACT analysis is based on the regulatory definitions of BACT, as well as EPA's current policy guidelines requiring a top-down approach. A BACT determination requires an analysis of the economic, environmental, and energy impacts of the proposed and alternative control technologies [see 40 CFR 52.21(b)(12); and Rule 62-212.200(40), and Rule 62-214.410, F.A.C.]. The analysis must, by definition, be specific to the Project (i.e., case-by-case).

### 4.2 NEW SOURCE PERFORMANCE STANDARDS

The applicable NSPS for CTs are codified in 40 CFR 60, Subpart GG and summarized in Appendix B. The applicable NSPS emission limit for NO<sub>x</sub> is 75 parts per million by volume dry (ppmvd) corrected for heat rate and 15 percent oxygen. For the CTs being considered

for the Project, the NSPS emission limit for NO<sub>x</sub> with the NSPS heat rate correction is 110.6 parts per million (ppm) on gas and 104.8 ppm on oil (corrected to 15 percent oxygen at a fuel-bound nitrogen content of 0.015 percent). The proposed NO<sub>x</sub> emission limits for the Project will be much lower than the NSPS.

### **4.3 BEST AVAILABLE CONTROL TECHNOLOGY**

#### **4.3.1 PROPOSED BACT**

In recent permitting actions, FDEP has established BACT for heavy-duty industrial gas turbines. These decisions have included the use of advanced dry low-NO<sub>x</sub> combustors for limiting NO<sub>x</sub> and CO emissions and clean fuels (natural gas and distillate oil) for control of other emissions, including SO<sub>2</sub>. The BACT proposed for the CTs is consistent with these FDEP permits. The proposed Project will have two modes of operation (see Section 2.3) for which a BACT analysis has been performed. The results of the analysis have concluded the following controls as BACT for the Project.

1. Natural Gas Fired. The CTs will utilize state-of-the-art dry low-NO<sub>x</sub> combustion technology which will achieve gas turbine exhaust NO<sub>x</sub> levels of no greater than 10 ppmvd corrected to 15 percent O<sub>2</sub>. CO emissions will be limited to 12 ppmvd at baseload.
2. Fuel Oil Fired. The CT will utilize water injection to achieve gas turbine exhaust NO<sub>x</sub> levels of no greater than 42 ppmvd corrected to 15 percent O<sub>2</sub>. CO emissions will be limited to 20 ppmvd at baseload.

#### **4.3.2 NITROGEN OXIDES**

##### **4.3.2.1 Introduction**

The BACT analysis was performed based on those available and feasible control technologies that can provide the maximum degree of emission reduction for emissions of NO<sub>x</sub>. An evaluation of the available and feasible control technologies determined that DLN combustion and DLN with water injection, for gas and oil combustion respectively, could provide the maximum degree of emission reduction. Other available technologies such as SCONO<sub>x</sub><sup>™</sup>, NO<sub>x</sub>Out, Thermal DeNO<sub>x</sub>, NSCR, and XONON<sup>™</sup> Combustion System were

evaluated and determined to be technically infeasible or not commercially demonstrated for the Project.

Available technologies for controlling NO<sub>x</sub> emissions from combustion turbines include combustion process modifications and post-combustion exhaust gas treatment systems. The BACT analysis for the Project was performed for the following alternatives:

1. Advanced dry low-NO<sub>x</sub> combustors at an emission rate of 10 ppmvd corrected to 15 percent O<sub>2</sub> when firing gas and 42 ppmvd corrected to 15 percent O<sub>2</sub> when firing oil.
2. Selective catalytic reduction (SCR) and advanced dry low-NO<sub>x</sub> combustors at an emission rate of approximately 3.5 ppmvd corrected to 15 percent O<sub>2</sub> when firing natural gas and 14.7 ppmvd corrected to 15 percent O<sub>2</sub> when firing oil.
3. SCONO<sub>x</sub><sup>™</sup>, using post combustion catalytic absorption to reduce emissions of NO<sub>x</sub>.
4. XONON<sup>™</sup>, using catalytic combustion to reduce emission of NO<sub>x</sub>.
5. Selective non-catalytic reduction (SNCR) which uses ammonia to reduce NO<sub>x</sub> but no catalyst.

SCONO<sub>x</sub><sup>™</sup>, XONON<sup>™</sup>, and SNCR are either not demonstrated and feasible or currently available. Appendix B presents a discussion of NO<sub>x</sub> control technologies and their feasibility for the Project.

Dry low-NO<sub>x</sub> combustor technology has recently been offered and installed by manufacturers to reduce NO<sub>x</sub> emissions by inhibiting thermal NO<sub>x</sub> formation through premixing fuel and air prior to combustion and providing staged combustion to reduce flame temperatures. NO<sub>x</sub> emissions from 25 ppmvd (corrected to 15-percent O<sub>2</sub>) and less has been offered by manufacturers for advanced combustion turbines. Advanced in this context is the larger (over 150 MW) and more efficient (higher initial firing temperatures and

lower heat rate) combustion turbines. This technology is truly pollution prevention since  $\text{NO}_x$  emissions are inhibited from forming.

SCR is a post-combustion process where  $\text{NO}_x$  in the gas stream is reacted with ammonia in the presence of a catalyst to form nitrogen and water. The reaction occurs typically between 600°F and 750°F, which has limited SCR application to combined cycle units where such temperatures occur in the HRSG. Exhausts from simple cycle operation reach up to 1,200°F, thus limiting SCR application for this mode of operation. With the higher cost ceramic catalyst, temperatures up to 1,050°F are possible. Such SCR systems are referred to as "hot" SCR. To accommodate "hot" SCR in the "F" Class gas turbine, some gas cooling would be required to maintain temperatures below 1,050°F. In-duct cooling using about 110,000 acfm of ambient air would maintain temperatures at below 1,050°F with turbine flow of about 2,600,000 acfm and up to 1,200°F. This could be accomplished with an electric powered fan rated at about 200 kW. While such modifications are theoretically possible, such gas cooling and its effectiveness has not been demonstrated on a "F" Class simple cycle gas turbine. SCR has been primarily installed and operated on combined cycle facilities using catalysts with temperature ranges from 600-750°F and generally achieving 9 ppmvd (corrected to 15-percent  $\text{O}_2$ ) or less while burning only natural gas.

Applications of SCR with oil firing are limited. Where oil firing has been attempted, catalyst poisoning and ammonium salt formation has occurred. Ammonium salts (ammonium sulfate and ammonium bisulfate) are formed by the reaction of sulfur oxides in the gas stream and ammonia. These salts are highly acidic, and special precautions in materials and ammonia injection rates must be implemented to minimize their formation. Ammonia injected in the SCR system that does not react with  $\text{NO}_x$  is emitted directly and referred to as ammonia slip. In general, SCR manufacturers guarantee ammonia slip to be no more than 10 ppmvd; however, permitted limits in some applications have exceeded 25 ppmvd. While SCR is technically feasible for the Project, SCR has not been applied to a simple cycle advanced combustion turbine of the size proposed for this Project or to the amount of oil firing that may occur.

For simple cycle projects, the predominate BACT emission rate has been based on DLN use when firing natural gas and water injection when firing distillate oil. Recent Florida projects include the IPS Vandolah Project, the Constellation Oleander Project, the IPS Shady Hills Project, the Reliant Holopaw Project, and the Jacksonville Electric Authority (JEA) Peaking Project. BACT emission rates for projects in Region IV have also been based on DLN and water injection. The BACT emission rates in Region IV for simple cycle projects have ranged from 9 to 15 ppmvd corrected to 15-percent O<sub>2</sub> when firing natural gas and 42 ppmvd corrected to 15-percent O<sub>2</sub> when firing distillate oil.

As discussed in Section 2.1, the proposed CTs will be fired primarily with natural gas. Distillate oil will be used as backup fuel not to exceed 720 hours per year. Table 4-1 presents a summary of emissions with dry low-NO<sub>x</sub> combustors and with dry low-NO<sub>x</sub> combustors and SCR assuming 39 percent operating capacity at an ambient temperature of 59°F. The NO<sub>x</sub> removed using SCR would be 140 TPY when firing oil and natural gas. The NO<sub>x</sub> removed when firing oil is based on 720 hours per year. The NO<sub>x</sub> removed when firing natural gas is based on 2,670 hours of operation.

**Technology Feasibility**—The proposed Project will use an advanced heavy-duty industrial gas turbine with advanced dry low-NO<sub>x</sub> combustors. This type of machine advances the state-of-the-art for CTs by being more efficient and less polluting than previous CTs. Integral to the machine's design is dry low-NO<sub>x</sub> combustors that prevent the formation of air pollutants within the combustion process, thereby eliminating the need for add-on controls that can have detrimental effects on the environment. An analogy of this technology is a more efficient automotive engine that gives better mileage and reduces pollutant formation without the need of a catalytic converter.

An advanced gas turbine is unique from an engineering perspective in two ways. First, the advanced machine is larger and has higher initial firing (i.e., combustion) temperatures than conventional turbines. This results in a larger, more thermally efficient machine. For



example, the electrical generating capability of the proposed GE Frame 7 FA advanced machine is about 170 MW compared to the 70 MW to 120 MW conventional machines. The higher initial firing temperature (i.e., 2,600°F) results in about 20 percent more electrical energy produced for the same amount of fossil fuel used in conventional machines. This has the added advantage of producing lower air pollutant emissions (e.g., NO<sub>x</sub>, PM, and CO) for each MW generated. While the increased firing temperature increases the thermal NO<sub>x</sub> generated, this NO<sub>x</sub> increase is controlled through combustor design.

The second unique attribute of the advanced machine is the use of dry low-NO<sub>x</sub> combustors that will reduce NO<sub>x</sub> emissions to 10 ppmvd when firing natural gas. Thermal NO<sub>x</sub> formation is inhibited by using staged combustion techniques where the natural gas and combustion air are premixed prior to ignition. This level of control will result in NO<sub>x</sub> emissions of about 0.04 lb/10<sup>6</sup> Btu, which is less than half of the emissions generated from conventional fossil fuel-fired steam generators.

Since the purpose of the Project is to produce electrical energy, and CT technology is rapidly advancing, it is appropriate to compare the proposed emissions on an equivalent generation basis to that of a conventional CT. The heat rate of the GE 7FA machines will be about 9,254 Btu/kWh (LHV, 59°F, natural gas). In contrast, the heat rate for a new conventional CT is about 11,000 Btu/kWh. Therefore, the amount of total NO<sub>x</sub> from the advanced CT will be more than 10-percent lower than a conventional turbine for the same amount of generation.

Also, the amount of NO<sub>x</sub> control achieved by the dry low-NO<sub>x</sub> combustor on an advanced CT is considerably higher than that achieved by a conventional CT. Because of the higher initial firing temperatures, the advanced CT results in greater NO<sub>x</sub> emission formation. Since the advanced machine has higher firing temperatures, the NO<sub>x</sub> emissions without the use of dry low-NO<sub>x</sub> combustion technology are much higher than a conventional CT (greater than 180 ppmvd vs. 150 ppmvd). This results in an overall greater NO<sub>x</sub> reduction on the advanced CT.

**Energy and Environmental Impacts** –The maximum predicted NO<sub>x</sub> impacts using the dry low-NO<sub>x</sub> technology are all considerably below the NO<sub>2</sub> PSD Class II increment of 25 µg/m<sup>3</sup>, annual average, and the AAQS of 100 µg/m<sup>3</sup>, annual average. Indeed, the maximum annual impact for the Project is 0.047 µg/m<sup>3</sup>, which is 5 percent of the significant impact level. While additional controls beyond dry low-NO<sub>x</sub> combustors (i.e., SCR and SCR with water injection) would reduce emissions, the effect will not be significant and much less than 1 percent of the PSD increment and the AAQS for the Project.

The use of dry low-NO<sub>x</sub> combustor technology is truly "pollution prevention". In contrast, use of SCR on the proposed Project will cause emissions of ammonia and ammonium salts, such as ammonium sulfate and bisulfate. Ammonia emissions associated with SCR are expected to be up to 10 ppm based on reported experience; previous permit conditions have specified this level. Indeed, ammonia emissions could be as high as 42.7 TPY/ per unit for the Project. Potential emissions of ammonium sulfate and bisulfate will increase emissions of PM<sub>10</sub> up to 20.8 TPY/per unit.

The electrical energy required to run the SCR system and the back pressure from the turbine will reduce the available power from the Project. The back pressure is a result of the amount of catalyst needed for the reduction and the velocity of exhaust gasses significantly reducing the available power. This power, which would otherwise be available to the electrical system, will have to be replaced by other less efficient units. The replacement power will cause air pollutant emissions that would not have occurred without SCR. These "secondary" emissions, coupled with potential emissions of ammonia and ammonium salts, will reduce the net benefit of "hot" SCR. The net reduction in emissions with SCR when all criteria pollutants are considered, will be 74.1 TPY. In addition to criteria pollutants, additional secondary emissions of carbon dioxide would be emitted. Indeed, the emissions including CO<sub>2</sub> would be greater with SCR than that proposed using dry low-NO<sub>x</sub> combustion technology.

The replacement of the SCR catalyst will create additional economic and environmental impacts since certain catalysts contain materials that are listed as hazardous chemical wastes under Resource Conservation and Recovery Act (RCRA) regulations (40 CFR 261). In addition, SCR will require the construction and maintenance of storage vessels of anhydrous or aqueous ammonia for use in the reaction. Ammonia has potential health effects, and the construction of ammonia storage facilities triggers the application of at least three major standards: Clean Air Act (section 112), Occupational Safety and Health Administration (OSHA) 29 CFR 1910.1000, and OSHA 29 CFR 1910.119.

**Economic Impacts**—An assessment of economic impacts was performed by assuming a baseline case of advanced DLN combustor technology and water injection with the addition of SCR controls. DLN and water injection technology provided by General Electric is expected to achieve a NO<sub>x</sub> exhaust concentration of 10 ppmvd and 42 ppmvd at 15 percent O<sub>2</sub> for gas and oil combustion in the turbine, respectively. SCR technology is expected to achieve NO<sub>x</sub> concentrations of 3.5 ppmvd at 15 percent O<sub>2</sub> for natural gas firing and 14.7 ppmvd @15 percent O<sub>2</sub> for oil firing.

The cost impact analysis was conducted using the OAQPS factors. Emission reductions were calculated assuming base load operations (2,670 hours of gas-firing at baseload, and 720 hours of oil firing). Specific capital and annual operating costs for the SCR control system are summarized in Tables B-3 and B-4 of Appendix B.

Cost effectiveness for the application of SCR technology to achieve 3.5 ppmvd at 15 percent O<sub>2</sub> was determined to be \$ 10,466 per ton of NO<sub>x</sub> removed. The total capital costs of SCR for the proposed plant are \$5,518,594 per CT. The total annualized cost of applying SCR with dry low-NO<sub>x</sub> combustion is \$1,462,292. This cost effectiveness accounts only for the reduction of NO<sub>x</sub> with SCR use and not the potential emissions from ammonia slip or other criteria pollutants that could result. The net control cost, considering maximum emission of ammonia slip, and additional PM and secondary emissions (from energy losses), is estimated at about \$19,760 per ton.

#### 4.3.2.2 Proposed BACT and Rationale

The proposed BACT for the Project is advanced dry low-NO<sub>x</sub> combustion technology. The proposed NO<sub>x</sub> emissions level using this technology is 10 ppmvd (corrected to 15 percent O<sub>2</sub>) when firing natural gas under baseload conditions. NO<sub>x</sub> from oil firing will be controlled using water injection (42 ppmvd corrected to 15 percent oxygen). This combination of the technology can achieve the maximum amount of emission reduction available, technically feasible and demonstrated for the Project. SCR is rejected based on the economic, environmental, and energy impacts. The proposed BACT is consistent with recent BACT decisions on other similar projects.

"Hot" SCR is rejected for the following reasons:

1. SCR was rejected based on technical, economic, environmental, and energy grounds. Table 4-1 summarizes these considerations which favor the dry low-NO<sub>x</sub> pollution prevention technology.
2. Hot SCR has not been demonstrated on an "F" Class CT. Applications of this technology on much smaller turbines have not been successful.
3. The estimated incremental cost of SCR is approximately \$10,466 per ton of NO<sub>x</sub> removed and is similar to cost for other projects that have rejected SCR as being unreasonable. This is even more apparent if additional pollutant emissions due to SCR are considered.
4. Additional environmental impacts would result from SCR operation, including emissions of ammonia; from secondary emissions (to replace the lost generation); and from the generation of hazardous waste (i.e., spent catalyst replacement). While NO<sub>x</sub> emissions would be reduced by about 140 TPY per unit with SCR, the net emissions reduction would not be as great. There are three additional factors that must be considered:
  - a. Ammonia slip would occur, and it may be as high as 42.7 TPY per unit.

- b. Additional particulate matter may be formed through the reaction of ammonia and sulfur oxides forming ammonium salts. As much as 20.8 TPY per unit additional particulate matter may be formed.
  - c. SCR will require energy for system operation and reduce the efficiency of the combustion turbine. This lost energy would have to be replaced since the proposed Project would be an efficient peaking power plant while operating. Any peaking power plants replacing this lost energy would be lower on the dispatch list and inevitably more polluting. Conservatively, this lost energy would result in the emissions of an additional 2.3 TPY of criteria pollutants. Additional emissions of carbon dioxide would also result.
  - d. The "net" cost effectiveness could be as high as \$19,760 per ton of pollutant removed.
5. The energy impacts of SCR will reduce potential electrical power generation by more than 2.0 million kilowatt hours (kWh) per year. This amount of energy is sufficient to provide the monthly electrical needs of 170 residential customers.
  6. The proposed BACT (i.e., dry low-NO<sub>x</sub> combustion) provides the most cost effective control alternative, is pollution preventing, and results in low environmental impacts (less than the significant impact levels). Dry low-NO<sub>x</sub> combustion at the proposed emissions levels has been adopted previously in BACT determinations. Indeed, compared to conventional CTs, the proposed BACT will result in 10 to 15 percent less NO<sub>x</sub> emission from the same amount of generation.

Significant energy penalties occur with SCR. With SCR, the output of the CT may be reduced by about 0.50 percent over that of advanced low-NO<sub>x</sub> combustors. This penalty is the result of the SCR pressure drop, which would be about 2.5 inches of water and would amount to about 1,773,648 kWh per year in potential lost generation. The energy required by the SCR equipment would be about 271,200 kWh per yr. Taken together, the total lost generation and energy requirements of SCR of 2,044,848 kWh per year could supply the monthly electrical needs of about 170 residential customers. To replace this lost energy, an

additional  $19.8 \times 10^{10}$  British thermal units per year (Btu/yr) or about 20 million cubic feet per year (ft<sup>3</sup>/yr) of natural gas would be required.

### 4.3.3 CARBON MONOXIDE

#### 4.3.3.1 Introduction

Emissions of CO are dependent upon the combustion design, which is a result of the manufacturer's operating specifications, including the air-to-fuel ratio, staging of combustion, and the amount of water injected (i.e., for oil firing). The CTs proposed for the Project have designs to optimize combustion efficiency and minimize CO as well as NO<sub>x</sub> emissions.

For the Project, the following alternatives were evaluated as BACT:

1. Combustion controls at 12 ppmvd when firing natural gas (at baseload) and 20 ppmvd when firing oil (at baseload); and
2. Oxidation catalyst at 90 percent removal; maximum annual CO emissions are 70.8 TPY per unit.

SCONO<sub>x</sub>™ also provides CO removal; however, it was not evaluated because, as discussed in Appendix B, it is not commercially demonstrated on "F"-Class turbines.

#### 4.3.3.2 Impact Analysis

**Economic**--The estimated annualized cost of a CO oxidation catalyst is \$534,770 per unit, resulting in a cost effectiveness of nearly \$8,400 per ton of CO removed. The cost effectiveness is based on 2,670 hours per year on natural gas and 720 hours per year of operation on oil. No costs are associated with combustion techniques since they are inherent in the design.

**Environmental**--Experience with similar projects indicate that the air quality impacts of both oxidation catalyst control and good combustion practice would be well below the significant impact levels for CO. Therefore, no significant environmental benefit would be realized by

the installation of a CO catalyst. Indeed, there would be additional particulate and secondary emissions as a result of an oxidation catalyst. The particulate would result from the conversion of SO<sub>2</sub> to sulfates, and the secondary emissions would result from the heat rate reduction as described below. Moreover, the air quality impacts at the proposed CT emission rate are predicted to be much less than the PSD significant impact levels. The maximum predicted CO impacts are less than 0.2 percent of the applicable ambient air quality standards (see Section 6). There would also be no secondary benefits, such as acidic deposition, associated with reductions of reducing CO using an oxidation catalyst.

**Energy**--An energy penalty would result from the pressure drop across the catalyst bed. A pressure drop of about 2 inches water gauge would be expected. At a catalyst back pressure of about 2 inches, an energy penalty of about 1,182,432 kWh/yr would result at 100 percent load. This energy penalty is sufficient to supply the electrical needs of about 99 residential customers for a year. To replace this lost energy, about  $1.1 \times 10^{10}$  Btu/yr or about 11 million ft<sup>3</sup>/yr of natural gas would be required.

#### 4.3.3.3 Proposed BACT and Rationale

Combustion design is proposed as BACT, as there are adverse technical and economic consequences of using catalytic oxidation on CTs. The proposed BACT emission rates for CO will not exceed 12 ppmvd when firing natural gas and 20 ppmvd when firing distillate oil at baseload conditions. Catalytic oxidation is considered unreasonable for the following reasons:

1. Catalytic oxidation will not produce measurable reduction in the air quality impacts;
2. The economic impacts are significant (i.e., the capital cost is about \$1.62 million per unit, with an annualized cost of \$534,770 per year per unit); and
3. Recent projects in Florida have been authorized with BACT emission limits of 25 ppmvd on gas and 90 ppmvd on oil.

Combustion design is proposed as BACT as a result of the technical and economic consequences of using catalytic oxidation on CTs. Catalytic oxidation is considered unreasonable since it will not produce a measurable reduction in the air quality impacts. Indeed, recent BACT decisions for similar advanced CTs have set limits in the 30 ppmvd range and higher. Even the Northeast States for Coordinated Air Use Management (NESCAUM) has recognized a BACT level of 50 ppmvd for CO emissions. The cost of an oxidation catalyst would be significant and not be cost effective given the maximum proposed emission limits.

#### 4.3.4 SO<sub>2</sub> AND H<sub>2</sub>SO<sub>4</sub> POLLUTANT EMISSIONS

There are no technically feasible methods for controlling the emissions of SO<sub>2</sub> and sulfuric acid mist from CTs, other than the inherent quality of the fuel. The use of flue gas desulfurization (FGD) systems are not available, technically feasible, demonstrated or cost effective on CTs using natural gas and very low sulfur distillate oil. Clean fuels, natural gas, and distillate oil represent BACT for these pollutants. The use of natural gas and very low sulfur (0.05 percent) fuel oil will limit emissions of SO<sub>2</sub>.

#### 4.3.5 PM/PM<sub>10</sub>, SO<sub>2</sub> AND OTHER REGULATED AND NONREGULATED POLLUTANT EMISSIONS

The PM/PM<sub>10</sub> emissions from the CTs are a result of incomplete combustion and trace elements in the fuel. The design of the CT ensures that particulate emissions will be minimized by combustion controls and the use of clean fuels. A review of EPA's BACT/LAER Clearinghouse Documents did not reveal any post-combustion particulate control technologies being used on gas- or oil-fired CTs.

The maximum particulate emissions from the CT will be lower in concentration than that normally specified for fabric filter designs {i.e., the grain loading associated with the maximum particulate emissions [about 10 pounds per hour (lb/hr) when firing natural gas]} is less than 0.01 grain per standard cubic foot (gr/scf), which is a typical design specification for a baghouse. This further demonstrates that no further particulate controls are necessary for the proposed Project.



There are no technically feasible methods for controlling the emissions of these pollutants from CTs, other than the inherent quality of the fuel. Clean fuels, natural gas and distillate oil represent BACT for these pollutants. The use of natural gas and very low sulfur (0.05%) fuel oil will limit emissions of SO<sub>2</sub>.

For the nonregulated pollutants, none of the control technologies evaluated for other pollutants (i.e., SCR) would reduce such emissions; thus, natural gas and distillate oil represent BACT because of their inherently low contaminant content.

Table 4-1. NO<sub>x</sub> Emission Estimates (TPY) of BACT Alternative Technologies (per Unit)

Alternative BACT Control Technologies	Operating Mode <sup>a</sup>		Total
	Oil	Gas	
<u>NO<sub>x</sub> Emission (TPY)</u>			
DLN/water injection only	122.4	92.5	215
DLN/water injection with SCR	42.9	32.3	75.2
Reduction	(79.5)	(60.2)	(139.8)
<u>Basis of Emissions (ppmvd)</u>			
DLN/water injection only	42	10	
DLN/water injection with "Hot" SCR	14.7	3.5	
Hours of Operation	720	2,670	3,390

Note: DLN = Dry low-NO<sub>x</sub>.  
 SCR = selective catalytic reduction.  
 TPY = tons per year.

<sup>a</sup> Emission rates were based on a "F" class combustion turbine operating at 100-percent capacity and firing natural gas for 2,670 hours and distillate fuel oil for 720 hours. Emission data are based on an ambient temperature of 59°F at maximum emission rates.

## 5.0 AMBIENT MONITORING ANALYSIS

The CAA requires that an air quality analysis be conducted for each criteria and noncriteria pollutant subject to regulation under the act before a major stationary source is constructed. Criteria pollutants are those pollutants for which AAQS have been established. Noncriteria pollutants are those pollutants that may be regulated by emission standards, but no AAQS have been established. This analysis may be performed by the use of modeling and/or by monitoring the air quality.

Based on the estimated emissions from the proposed Project (see Table 3-3), preconstruction ambient monitoring analyses for SO<sub>2</sub>, PM<sub>10</sub>, NO<sub>2</sub>, CO, and sulfuric acid mist are required to be submitted as part of the application. A major source may waive the ambient monitoring analysis requirement if it can be demonstrated that the proposed source's maximum air quality impacts will not exceed the PSD *de minimis* concentration levels.

As shown in Table 3-4, the proposed Project's impacts are predicted to be below the applicable *de minimis* monitoring concentrations for all pollutants. For sulfuric acid mist, which is a noncriteria pollutant, although the Project's emissions are greater than the significant emission rate, EPA has established no acceptable monitoring method for this pollutant. Therefore, Peace River Station, L.L.C. requests an exemption from the preconstruction monitoring requirement for sulfuric acid in accordance with the PSD regulations.

## 6.0 AIR QUALITY IMPACT ANALYSIS

### 6.1 SIGNIFICANT IMPACT ANALYSIS APPROACH

The modeling approach followed EPA and DEP modeling guidelines for determining compliance with AAQS and PSD increments. For all applicable pollutants that have emission increases that will exceed the PSD significant emission rate due to the proposed Project, a significant impact analysis was performed. This analysis determines whether the Project alone will result in predicted impacts that will exceed the EPA significant impact levels in any areas beyond the Project's fenced property.

If the Project's impacts are above the significant impact levels, then a more detailed air modeling analysis that includes background sources is required. If the Project's impacts are below the significant impact levels, a more detailed air modeling analysis is not required.

Generally, if a new project also is within 200 km of a PSD Class I area, then a significant impact analysis is also performed for the PSD Class I area. EPA has proposed PSD Class I significant impact levels that have not been finalized as of this report (see Section 3.2.3).

Because the proposed Project site is approximately 124 km from the Chassahowitzka National Wilderness Area PSD Class I area, a significant impact modeling analysis has been performed. Air impact analyses were not performed for other PSD Class I areas since they are located more than 200 km from the Project.

### 6.2 PRECONSTRUCTION MONITORING ANALYSIS APPROACH

The modeling approach followed EPA and DEP modeling guidelines for evaluating a project's impacts relative to the *de minimis* monitoring levels to determine the need to submit ambient monitoring data prior to construction. Current DEP policies stipulate that the highest annual average and highest short-term concentrations are to be compared to the applicable *de minimis* monitoring levels.

### 6.3 AIR MODELING ANALYSIS APPROACH

#### 6.3.1 GENERAL PROCEDURES

As stated in the previous sections, for each pollutant which is emitted above the significant emission rate, air modeling analyses are required to determine if the Project's impacts are predicted to be greater than the significant impact levels and *de minimis* monitoring levels. These analyses consider the Project's impacts alone. Air quality impacts are predicted using 5 years of meteorological data and selecting the highest predicted ground-level concentrations for comparison to the significant impact levels and *de minimis* monitoring levels.

If the Project's impacts are greater than the significant impact levels, the air modeling analyses must consider other nearby sources and background concentrations, and predict concentration for comparison to ambient standards. Because the Project's maximum impacts are predicted to be less than the significant impact levels, only the highest concentrations due to the Project's emissions were evaluated.

To develop the maximum short-term concentrations for the proposed Project, the modeling approach was divided into screening and refined phases to reduce the computation time required performing the modeling analysis. Concentrations are predicted for the screening phase using a coarse receptor grid and a 5-year meteorological data record. If the highest concentration is predicted at a receptor in an area where the receptor spacing is more than 100 m, then a refined analysis is performed. Modeling refinements are performed using a receptor spacing of 100 m with a receptor grid centered on the screening receptor at which the maximum concentration was predicted. The air dispersion model is then executed with the refined grid for the entire year of meteorology during which the screening concentration occurred.

More detailed descriptions of the model, along with the emission inventory, meteorological data, and receptor grids are presented in the following sections.

### 6.3.2 MODEL SELECTION

The selection of an air quality model to calculate air quality impacts for this Project was based on its applicability to simulate impacts in areas surrounding the Project as well as at the PSD Class I area of the Chassahowitzka NWA, located about 124 km from the Site. Two air quality dispersion models were selected and used in these analyses to address air quality impacts for the Project. These models were:

- The Industrial Source Complex Short Term (ISCST3) dispersion model, and
- The California Puff model (CALPUFF)

The Industrial Source Complex Short-term (ISCST3, Version 99155) dispersion model (EPA, 1999) was used to evaluate the pollutant impacts due to the Project in nearby areas surrounding the Site. This model is maintained by the EPA on its Internet website, Support Center for Regulatory Air Models (SCRAM), within the Technical Transfer Network (TTN). A listing of ISCST3 model features is presented in Table 6-1. The ISCST3 model is designed to calculate hourly concentrations based on hourly meteorological data (i.e., wind direction, wind speed, atmospheric stability, ambient temperature, and mixing heights). The ISCST3 model is applicable to sources located in either flat or rolling terrain where terrain heights do not exceed stack heights. These areas are referred to as simple terrain. The model can also be applied in areas where the terrain exceeds the stack heights. These areas are referred to as complex terrain.

The Site is about 130 ft above mean sea level (msl). Around the immediate vicinity of the Site, the terrain is flat to gently rolling with elevations that range within 10 to 20 ft of the Site elevation.

Since the proposed stack heights for the CTs are proposed to be 60 ft, the surrounding terrain is below the proposed stack top heights. Therefore, the surrounding terrain can be considered as simple (i.e., less than stack top) with respect to the proposed stack heights. Due to the minimal amount of terrain elevation differences in the Project's vicinity, receptor elevations were not included in the analysis. As a result, the simple terrain option was used

for the air modeling analysis which assumes that all receptors are at the same elevation as the stack base elevations for the CTs.

In this analysis, the EPA regulatory default options were used to predict all maximum impacts. The ISCST3 model can run in the rural or urban land use mode that affects stability dispersion coefficients, wind speed profiles, and mixing heights. Land use can be characterized based on a scheme recommended by EPA (Auer, 1978). If more than 50 percent land use within a 3-km radius around a project is classified as industrial or commercial, or high-density residential, then the urban option should be selected. Otherwise, the rural option is appropriate. Based on the land-use within a 3-km radius of the proposed Site (see Figure 1-1), the rural dispersion coefficients were used in the modeling analysis.

The ISCST3 model was used to provide maximum concentrations for the annual and 24-, 8-, 3-, and 1-hour averaging times. To estimate impacts due to emissions from the CT stacks, an emission rate of 79.365 pounds per hour (lb/hr) or 10 grams per second (g/s) was initially used to produce relative concentrations as a function of the modeled emission rate (i.e.,  $\mu\text{g}/\text{m}^3$  per 10 g/s). These impacts are referred to as generic pollutant impacts. Maximum air quality impacts for specific pollutants were then determined by multiplying the maximum pollutant-specific emission rate in lb/hr (g/s) to the maximum predicted generic impact divided by 79.365 lb/hr (10 g/s).

At distances beyond 50 km from a source, the CALPUFF model, Version 5.0 (EPA, 1998), is recommended for use by the EPA and DEP. The CALPUFF model is a long-range transport model applicable for estimating the air quality impacts in areas that are more than 50 km from a source. The methods and assumptions used in the CALPUFF model were based on the latest recommendations for modeling analysis as presented in the Interagency Workgroup on Air Quality Models (IWAQM), Phase 2 Summary Report and Recommendations for Modeling Long Range Transport Impacts (EPA, 1998). This model is also maintained by the EPA on the SCRAM website.

As a result, the CALPUFF model was used to perform the significant impact analysis for the Project at the Class I area of the Chassahowitzka NWA. The CALPUFF model was also used to assess the Project's impact on regional haze at the Class I area (see Section 7.0). Based on discussions with DEP, the ISCST3 model was used to determine the "worst-case" operating load and ambient temperature that produced the Project's maximum impact at the Class I area. Based on that analysis, air quality impacts were then predicted with the CALPUFF model using the "worst-case" operating scenario to compare the Project's impacts to Class I significant impact levels and potential contribution to regional haze. A more detailed description of the assumptions and methods used for the CALPUFF model is presented in Appendix C.

### 6.3.3 METEOROLOGICAL DATA

Meteorological data used in the ISCST3 model to determine air quality impacts consisted of a concurrent 5-year period of hourly surface weather observations and twice-daily upper air soundings from the National Weather Service (NWS) stations at Tampa International Airport and Ruskin, Florida, respectively. The 5-year period of meteorological data was from 1987 through 1991, which are the latest readily available data for these stations that are acceptable to the Florida DEP. The NWS station at Tampa is located approximately 77 km (48 miles) west-northwest of the proposed Site while the NWS station at Ruskin is located approximately 65 km (39 miles) west of the proposed Site.

These meteorological data are the most complete and representative of the region around the Project Site because both the Site and the weather stations are located in areas that experience similar weather conditions, such as frontal passages. In addition, these data have been approved for use by the Florida DEP in previous air permit applications to address air quality impacts for other proposed sources locating in Polk County and adjacent counties.

For the CALPUFF model, additional meteorological parameters are needed (e.g., precipitation, relative humidity) to predict air quality concentrations than that required for



the ISCST3 model. More detailed descriptions of the assumptions and methods used for processing the meteorological data and establishing the model domain are presented in Appendix C.

#### **6.3.4 EMISSION INVENTORY**

A summary of the criteria pollutant emission rates, physical stack and stack operating parameters for the proposed CTs used in the air modeling analysis is presented in Tables 2-1 and 2-2. The emission and stack operating parameters presented for 32°F and 95°F ambient temperatures for both natural gas and distillate fuel oil were used in the modeling to determine the maximum air quality impacts for a range of possible operating conditions.

Six modeling scenarios per fuel type were considered:

1. base operating load for the ambient temperature of 32°F and 95°F;
2. 75 percent operating load for the ambient temperature of 32°F and 95°F; and
3. 50 percent operating load for the ambient temperature of 32°F and 95°F;

The proposed CTs will have a stack height of 60 feet and an inner stack diameter of 22 ft. Because the proposed CT stack heights are less than GEP, building downwash effects were included in the modeling analysis (see following section on building downwash).

#### **6.3.5 RECEPTOR LOCATIONS**

For predicting maximum concentrations in the vicinity of the plant, a polar receptor grid comprised of 136 grid receptors was used. These receptors included 52 receptors located on radials extending out from the proposed CTs' stack locations. Along each radial, receptors were located at the plant property and downwind distances of:

- 0.3 to 3.0 km at 100 meter spacing
- 3.0 to 6.0 km at 250 meter spacing;
- 6.0 to 10.0 km at 500 meter spacing; and
- 10.0 to 20.0 km at 1 km spacing.

The polar receptor grid was centered on the middle CT stack of the three proposed CT stacks.

Modeling refinements were performed for the worst-case loads for fuel oil only, by employing a polar receptor grid with a maximum spacing of 100 m along each radial and an angular spacing between radials of 0.25 to 2 degrees.

Since the terrain surrounding the proposed plant site varies little from the stack base elevation of 130 ft-msl, the terrain was assumed to be flat and receptor elevations were set equal to the stack base elevation.

To address impacts in the Chassahowitzka NWA, the following receptor locations were used:

Receptors at the PSD Class I Area of the  
Chassahowitzka National Wilderness Area

UTM Coordinates (m)

East	North
340,300	3,165,700
340,300	3,167,700
340,300	3,169,800
340,700	3,171,900
342,000	3,174,000
343,000	3,176,200
343,700	3,178,300
342,400	3,180,600
341,100	3,183,400
339,000	3,183,400
336,500	3,183,400
334,000	3,183,400
331,500	3,183,400

Note: UTM Zone 17

These receptors have been used in previous PSD applications that addressed predicting impacts in the Chassahowitzka NWA. The Project's East and North UTM coordinates are 419.5 and 3,069.7 km, respectively, in Zone 17.

### 6.3.6 BUILDING DOWNWASH EFFECTS

A review of the dimensions of structures proposed for the Project was conducted to determine those structures that could produce building downwash effects. The only significant structures in the vicinity of the proposed CT stacks are the proposed CT air filter inlets, CT structures, and oil tanks. Because the heights of other structures, such as the administration building, are less than 20 ft and would not produce downwash effects for the Project's emissions, they were not considered in the analysis.

The height and widths of these structures are as follows:

<u>Structure</u>	<u>Height (ft)</u>	<u>Width (ft)</u>	<u>Length (ft)</u>
CT air inlet	47	36	36
CT structure	22	30	42
Fuel Oil Tanks (2)	48	80 (Dia)	Not applicable

Building dimensions for the project's structures were entered into the EPA's Building Profile Input Program (BPIP, Version 95086) for the purpose of obtaining direction-specific building heights and widths for all downwash-affected sources. The direction-specific building dimensions were then input to the ISCST3 model as the building height and width for each of 36 ten-degree wind sectors. A summary of the direction-specific building dimensions used in the modeling is presented in Appendix D.

## 6.4 SIGNIFICANT IMPACT ANALYSIS RESULTS

### 6.4.1 SITE VICINITY

The modeling analysis results for the proposed CTs alone in the vicinity of the plant are summarized in Tables 6-2 and 6-3. The maximum pollutant concentrations predicted in the screening analysis for three CTs firing natural gas and distillate fuel oil for the three CTs at the three operating loads and two ambient temperatures are presented in Tables 6-2. The maximum pollutant concentrations predicted in the refined analysis for three CTs firing distillate fuel oil are presented in Tables 6-3. Since the air impacts in the screening analysis showed that the Project's impacts firing natural gas were lower than those predicted for firing oil, the refined analysis was only performed for the Project firing oil.

As shown in the tables, the maximum predicted PM, SO<sub>2</sub>, NO<sub>x</sub>, and CO impacts due to the proposed CTs are all below the significant impact levels. Because the proposed source will not have a significant impact upon the air quality in the vicinity of the plant site, more detailed modeling analyses for determining compliance with the AAQS and allowable PSD Class II increments are not required.

The maximum predicted PM, SO<sub>2</sub>, NO<sub>x</sub>, and CO impacts due to the proposed CTs are also below the *de minimis* monitoring levels. Because the proposed source will not have predicted impacts greater than *de minimis* levels, preconstruction monitoring data are not required to be submitted as part of the PSD review.

A summary of the model results for the ISCST3 model is presented in Appendix E. The locations of the maximum predicted concentrations are also given in the summary. Model input files are also provided in Appendix E.

### 6.4.2 PSD CLASS I AREA

The modeling analysis results for the proposed CTs alone at the PSD Class I area of the Chassahowitzka NWA are summarized in Tables 6-4 and 6-5. The maximum pollutant concentrations predicted in the screening analysis for three CTs firing natural gas and

distillate fuel oil at the three operating loads and two ambient temperatures are presented in Table 6-4.

As shown in Table 6-4, the "worst-case" operating load and ambient temperature that produced the Project's maximum for SO<sub>2</sub> and NO<sub>2</sub> impacts at the Class I area occurred for baseload operation with an ambient temperature of 32°F; for PM<sub>10</sub>, the "worst-case" operating load and ambient temperature was at 50 percent load and 95°F. As a result, air quality impacts for the Project were predicted at the Class I area with the CALPUFF model using these "worst-case" operating scenarios for the applicable pollutant. A summary of the overall maximum concentrations predicted at the Class I area due to the Project's emissions is given in Table 6-5 for comparison to the PSD Class I significant impact levels and increments. Results are provided both for the ISCST3 and CALPUFF models.

As shown in Table 6-5, the maximum PM, SO<sub>2</sub>, and NO<sub>2</sub> impacts due to the Project are all below the significant impact levels. Because the Project will not have a significant impact upon the air quality at the Class I area, more detailed modeling analyses for determining compliance with the PSD Class I increments are not required. These maximum concentrations due to the Project are predicted to be less than 1 percent of the PSD Class I increments.

A summary of the model results for the ISCST3 and CALPUFF models is presented in Appendix E. The locations of the maximum predicted concentrations are also given in the summary. Model input files are also provided in Appendix E.

Table 6-1. Major Features of the ISCST3 Model

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**ISCST3 Model Features**

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- Polar or Cartesian coordinate systems for receptor locations
- Rural or one of three urban options which affect wind speed profile exponent, dispersion rates, and mixing height calculations
- Plume rise due to momentum and buoyancy as a function of downwind distance for stack emissions (Briggs, 1969, 1971, 1972, and 1975; Bowers, et al., 1979).
- Procedures suggested by Huber and Snyder (1976); Huber (1977); and Schulman and Scire (1980) for evaluating building wake effects
- Procedures suggested by Briggs (1974) for evaluating stack-tip downwash
- Separation of multiple emission sources
- Consideration of the effects of gravitational settling and dry deposition on ambient particulate concentrations
- Capability of simulating point, line, volume, area, and open pit sources
- Capability to calculate dry and wet deposition, including both gaseous and particulate precipitation scavenging for wet deposition
- Variation of wind speed with height (wind speed-profile exponent law)
- Concentration estimates for 1-hour to annual average times
- Terrain-adjustment procedures for elevated terrain including a terrain truncation algorithm for ISCST3; a built-in algorithm for predicting concentrations in complex terrain
- Consideration of time-dependent exponential decay of pollutants
- The method of Pasquill (1976) to account for buoyancy-induced dispersion
- A regulatory default option to set various model options and parameters to EPA recommended values (see text for regulatory options used)
- Procedure for calm-wind processing including setting wind speeds less than 1 m/s to 1 m/s.

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Note: ISCST3 = Industrial Source Complex Short-Term.  
Source: EPA, 1995.

Table 6-2. Maximum Pollutant Concentrations Predicted for Three Simple-Cycle Combustion Turbines Firing Natural Gas and Distillate Fuel Oil by Operating Load and Inlet Ambient Temperature

Pollutant	Averaging Time	Maximum Predicted Concentrations (ug/m <sup>3</sup> ) by Operating Load and Air Temperature (1)					
		Base Load		75% Load		50% Load	
		32°F	95°F	32°F	95°F	32°F	95°F
<b>Natural Gas</b>							
SO <sub>2</sub>	Annual	0.0068	0.0065	0.0066	0.0061	0.0063	0.0057
	24-Hour	0.086	0.083	0.082	0.076	0.076	0.070
	3-Hour	0.398	0.357	0.336	0.338	0.421	0.366
PM10	Annual	0.0072	0.0078	0.0084	0.0092	0.0107	0.0113
	24-Hour	0.091	0.098	0.105	0.114	0.128	0.138
NO <sub>x</sub>	Annual	0.047	0.045	0.045	0.042	0.044	0.040
CO	8-Hour	0.65	0.60	0.59	0.56	0.63	0.70
	1-Hour	2.8	2.6	2.6	2.4	2.7	2.8
<b>Distillate Fuel Oil</b>							
SO <sub>2</sub>	Annual	0.068	0.065	0.066	0.061	0.062	0.058
	24-Hour	0.87	0.82	0.82	0.76	0.75	0.71
	3-Hour	4.1	3.7	3.4	3.5	4.2	3.7
PM10	Annual	0.0141	0.0149	0.0166	0.0179	0.0210	0.0229
	24-Hour	0.179	0.186	0.208	0.223	0.254	0.276
NO <sub>x</sub>	Annual	0.23	0.21	0.22	0.20	0.20	0.19
CO	8-Hour	1.28	1.17	1.15	1.09	1.26	1.43
	1-Hour	5.5	5.0	5.0	4.8	5.5	5.6

(1) Concentrations are based on highest predicted concentrations using five years of meteorological for 1987 to 1991 of surface and upper air data from the National Weather Service stations at Tampa International Airport and Ruskin, respectively.

$$109/5 = 79.37 \text{ lb/hr}$$

$$\frac{\text{E rate lb/hr}}{79.37 \text{ lb/hr}} \times \text{generic model} = \text{Conc. (ug/m}^3\text{)}$$

Table 6-3. Summary of Maximum Pollutant Concentrations Predicted for Three Simple-Cycle Combustion Turbines Compared to the EPA Class II Significant Impact Levels, PSD Class II Increments, and AAQS

Pollutant	Averaging Time	Maximum Concentration (ug/m <sup>3</sup> )		EPA Class II Significant Impact Levels (ug/m <sup>3</sup> )	PSD Class II Increments (ug/m <sup>3</sup> )	AAQS (ug/m <sup>3</sup> )
		Natural Gas	Fuel Oil (a)			
SO <sub>2</sub>	Annual	0.0068	0.071	1	25	60
	24-Hour	0.086	0.96	5	91	260
	3-Hour	0.42	4.2	25	512	1,300
PM10	Annual	0.0113	0.234	1	17	50
	24-Hour	0.138	0.28	5	30	150
NO <sub>x</sub>	Annual	0.047	0.23	1	25	100
CO	8-Hour	0.70	1.4	500	NA	10,000
	1-Hour	2.8	5.6	2,000	NA	40,000

NA = not applicable

(a) Refined modeling values



Table 6-4. Maximum Pollutant Concentrations Predicted for Three Simple-Cycle Combustion Turbines Firing Natural Gas and Distillate Fuel Oil by Operating Load and Inlet Ambient Temperature at the PSD Class I Area of the Chassahowitzka NWA

Pollutant	Averaging Time	Maximum Predicted Concentrations (ug/m <sup>3</sup> ) by Operating Load and Air Temperature (1)					
		Base Load		75% Load		50% Load	
		32°F	95°F	32°F	95°F	32°F	95°F
<b>Natural Gas</b>							
SO <sub>2</sub>	Annual	0.00121	0.00113	0.00112	0.00103	0.00101	0.00089
	24-Hour	0.019	0.017	0.019	0.017	0.017	0.015
	3-Hour	0.122	0.111	0.108	0.096	0.091	0.080
PM10	Annual	0.0013	0.0013	0.0014	0.0015	0.0017	0.0018
	24-Hour	0.020	0.021	0.024	0.026	0.028	0.030
NO <sub>x</sub>	Annual	0.00832	0.00778	0.00775	0.00708	0.00695	0.00614
<b>Distillate Fuel Oil</b>							
SO <sub>2</sub>	Annual	0.0122	0.0114	0.0112	0.0104	0.0100	0.0090
	24-Hour	0.190	0.176	0.187	0.172	0.166	0.152
	3-Hour	1.23	1.14	1.08	0.97	0.90	0.81
PM10	Annual	0.003	0.003	0.003	0.003	0.003	0.004
	24-Hour	0.039	0.040	0.047	0.050	0.056	0.059
NO <sub>x</sub>	Annual	0.040	0.037	0.037	0.034	0.033	0.030

(1) Concentrations are based on highest predicted concentrations using five years of meteorological for 1987 to 1991 of surface and upper air data from the National Weather Service stations at Tampa International Airport and Ruskin, respectively.

Table 6-5. Summary of Maximum Pollutant Concentrations Predicted for Three Simple-Cycle Combustion Turbines Compared to the EPA Class I Significant Impact Levels and PSD Class I Increments

Pollutant	Averaging Time	Maximum Concentration (ug/m <sup>3</sup> )		EPA Class I Significant Impact Levels (ug/m <sup>3</sup> )	PSD Class I Increments (ug/m <sup>3</sup> )
		ISCST	CALPUFF		
<b><u>Natural Gas</u></b>					
SO <sub>2</sub>	Annual	0.0012	0.0007	0.1	2
	24-Hour	0.019	0.012	0.2	5
	3-Hour	0.122	0.045	1.0	25
PM10	Annual	0.0018	0.0009	0.2	4
	24-Hour	0.030	0.017	0.3	8
NO <sub>x</sub>	Annual	0.008	0.0009	0.1	2.5
<b><u>Distillate Fuel Oil</u></b>					
SO <sub>2</sub>	Annual	0.012	0.007	0.1	2
	24-Hour	0.19	0.12	0.2	5
	3-Hour	1.23	0.46	1.0	25
PM10	Annual	0.004	0.002	0.2	4
	24-Hour	0.059	0.033	0.3	8
NO <sub>x</sub>	Annual	0.040	0.004	0.1	2.5

## 7.0 ADDITIONAL IMPACT ANALYSIS

### 7.1 IMPACTS DUE TO DIRECT GROWTH

The Peace River Station Project is being constructed to meet current and projected electric demands. Additional growth as a direct result of the additional electric power provided by the Project is not expected.

Construction of the Project will occur over an 18-month period requiring an average of approximately 25 workers during that time. It is anticipated that many of these construction personnel will commute to the Site.

The Peace River Station will employ a total of 12 operational workers at Project build-out. The operational workforce will also include annual contracted maintenance workers to be hired for periodic routine services. The workforce needed to operate the proposed Project represents a small fraction of the population already present in the immediate area. Therefore, while there would be a small increase in vehicular traffic in the area, the effect on air quality levels would be minimal.

There are also expected to be no air quality impacts due to associated industrial/ commercial growth given the Site's location relative to the City of Fort Meade. The existing commercial infrastructure should be adequate to provide any support services that the Project might require.

### 7.2 IMPACT ON SOILS, VEGETATION, WILDLIFE, AND VISIBILITY IN THE PROJECT'S VICINITY

Because the Project's impacts on the local air quality are predicted to be less than the significant impact levels for PSD Class II areas, the Project's impacts on soils, vegetation, and wildlife in the Project's vicinity are also not expected to be significant. According to the modeling results presented in Section 6.0, the maximum air quality impacts due to the Project are predicted to be

well below the PSD Class II significant impact levels, PSD Class II Increments, and AAQS. In addition, no visibility impairment in the Project's vicinity is expected due to the types and quantities of emissions proposed for the Project. The opacity of the proposed CT exhaust emissions will be 10 percent or less.

According to the USDA Polk County Soil Survey, soils in the vicinity of the Site are classified as Tavares fine sand, 0 to 5 percent slopes. Tavares fine sand is described as moderately well drained soils that formed in sandy marine sediments and are found on broad uplands and knolls within flatwoods (Polk County Soil Survey, USDA 1980). These soils can be described as strongly acid. The pollutants emitted by the Project that could cause potential impact to soils are SO<sub>2</sub> and NO<sub>x</sub>. The primary effect of SO<sub>2</sub> and NO<sub>x</sub> deposition and adsorption by soils is the resultant lowering of soil pH. Low soil pH will have an influence on most chemical and biological reactions in the soil including the level and availability of most plant nutrients in the soil. Based on the extremely low SO<sub>2</sub> and NO<sub>2</sub> impacts predicted for the Project and the ambient acidic nature of the soils, the Project's emissions will not have any significant adverse impact to soils at the Site or vicinity.

Although air pollution impacts to wildlife have been reported in the literature, many of the incidents involved acute exposures to pollutants, usually caused by unusual or highly concentrated releases or unique weather conditions. Generally, there are three ways pollutants may affect wildlife: through inhalation, through exposure with skin, and through ingestion (Newman 1980). Ingestion is the most common means and can occur through eating or drinking of high concentrations of pollutants. Bioaccumulation is the process of animals collecting and accumulating pollutant levels in their bodies over time. Other animals that prey on these animals would then be ingesting concentrated pollutant levels.

It is unlikely that the Project's emissions will cause injury or death to wildlife based on a review of the limited literature on air pollutant effects on wildlife. The Project's impacts are predicted

to be very low and dispersed over a large area. Coupled with the mobility of wildlife, the potential for exposure of wildlife to the Project's impacts under weather conditions that lead to high concentrations is extremely unlikely.

The maximum concentrations of SO<sub>2</sub>, PM<sub>10</sub>, NO<sub>2</sub>, and CO due to the Project's emissions are predicted to be at least an order of magnitude lower than the EPA Class II significant impact levels; therefore, no significant impacts associated with facility operations are expected. The maximum predicted concentrations are less than one percent of the AAQS. Since the AAQS are designed to protect the public welfare, including effects on soils, vegetation and wildlife, no detrimental effects on soils, vegetation or wildlife should occur in this area.

Visibility impairment in the Project's vicinity is not expected due to the types and quantities of emissions proposed for the Project. The opacity of the proposed CT exhaust emissions will be 10 percent or less.

### **7.3 IMPACTS UPON PSD CLASS I AREAS**

#### **7.3.1 IDENTIFICATION OF AQRVS AND METHODOLOGY**

The Peace River Station is located about 124 km from the PSD Class I area of the Chassahowitzka NWA. Other PSD Class I areas are located more than 200 km from the Site. Because the proposed Project will be fired primarily with natural gas, a clean fuel, with low sulfur content distillate fuel oil as a backup fuel, it is expected that the Project's impacts for SO<sub>2</sub>, NO<sub>2</sub>, and PM<sub>10</sub> will be minimal and not significantly affect or impair visibility or soils and vegetation at the Class I areas.

An AQRV analysis was conducted to assess the potential risk to AQRVs of the Chassahowitzka NWA due to the proposed emissions from the Project. The U.S. Department of the Interior in 1978 administratively defined AQRVs to be:

All those values possessed by an area except those that are not affected by changes in air quality and include all those assets of an area whose vitality, significance, or integrity is dependent in some way upon the air environment. These values include visibility and those scenic, cultural, biological, and recreational resources of an area that are affected by air quality.

Important attributes of an area are those values or assets that make an area significant as a national monument, preserve, or primitive area. They are the assets that are to be preserved if the area is to achieve the purposes for which it was set aside (Federal Register 1978).

Except for visibility, AQRVs were not specifically defined. However, odor, soil, flora, fauna, cultural resources, geological features, water, and climate generally have been identified by land managers as AQRVs. Since specific AQRVs have not been identified for the Chassahowitzka NWA, this AQRV analysis evaluates the effects of air quality on general vegetation types and wildlife found in the Chassahowitzka NWA.

Vegetation type AQRVs and their representative species types have been defined by the U.S. Fish and Wildlife as:

Marshlands - black needlerush, saw grass, salt grass, and salt marsh cordgrass

Marsh Islands - cabbage palm and eastern red cedar

Estuarine Habitat - black needlerush, salt marsh cordgrass, and wax myrtle

Hardwood Swamp - red maple, red bay, sweet bay, and cabbage palm

Upland Forests - live oak, scrub oak, longleaf pine, slash pine, wax myrtle, and saw palmetto

Mangrove Swamp - red, white, and black mangrove

Wildlife AQRVs have been identified as endangered species, waterfowl, marsh and waterbirds, shorebirds, reptiles, and mammals.

The maximum pollutant concentrations due to the Project's emissions predicted at the PSD Class I area of the Chassahowitzka NWA are presented in Table 7-1. These results are based on using the CALPUFF model (see Section 6.0).

Similar to the evaluation performed in Section 7.2, a screening approach was used that compared the maximum ambient concentration of air pollutants of concern due to the Project's emissions at the PSD Class I area of the Chassahowitzka NWA with effect threshold limits for both vegetation and wildlife as reported in the scientific literature. A literature search was conducted that specifically addressed the effects of air contaminants on plant species reported to occur in the NWA. While the literature search focused on such species as cabbage palm, eastern red cedar, lichens, and species of the hardwood swamplands and mangrove forest, no specific citations that addressed these species were found. It is recognized that effect threshold information is not available for all species found in the Chassahowitzka NWA, although studies have been performed on a few of the common species and on other similar species that can be used as indicators of effects.

### 7.3.2 IMPACTS TO SOILS

For soils, the potential and hypothesized effects of atmospheric deposition include:

- Increased soil acidification,
- Alteration in cation exchange,
- Loss of base cations, and
- Mobilization of trace metals.

The potential sensitivity of specific soils to atmospheric inputs is related to two factors. First, the physical ability of a soil to conduct water vertically through the soil profile is important in influencing the interaction with deposition. Second, the ability of the soil to resist chemical changes, as measured in terms of pH and soil cation exchange capacity (CEC), is important in determining how a soil responds to atmospheric inputs.

According to the USDA Soil Surveys of Citrus and Hernando Counties, nine soil complexes are found in the Chassahowitzka NWA. These include Aripeka fine sand, Aripeka-Okeelanta-Lauderhill, Hallendale-Rock outcrop, Homosassa mucky fine sandy loam, Lacoche, Okeelanta mucks, Okeelanta-Lauderdale-Terra Ceia mucks, Rock outcrop-Homosassa-Lacochee, and Weekiwachee-Durbin mucks (Porter, 1996). The majority of the soil complexes found in the NWA are inundated by tidal waters, contain a relatively high organic matter content, and have high buffering capacities based on their CEC, base saturation, and bulk density. The regular flooding of these soils by the Gulf of Mexico regulates the pH and any change in acidity in the soil would be buffered by this activity. Therefore, they would be relatively insensitive to atmospheric inputs. However, Terra Ceia, Okeelanta, and Lauderdale freshwater mucks are present along the eastern border of the NWA, and may be more sensitive to atmospheric sulfur deposition (Porter, 1996). Although not tidally influenced, these freshwater mucks are highly organic and therefore have a relatively high intrinsic buffering capacity.

The relatively low sensitivity of the soils to atmospheric inputs coupled with the extremely low ground-level concentrations of contaminants projected for the Chassahowitzka NWA from the proposed Project's emissions precludes any significant impact on soils.

### 7.3.3 IMPACTS TO VEGETATION

In general, the effects of air pollutants on vegetation occur primarily from SO<sub>2</sub>, NO<sub>2</sub>, O<sub>3</sub>, and PM. Effects from minor air contaminants, such as fluoride, chlorine, hydrogen chloride, ethylene, ammonia, hydrogen sulfide, CO, and pesticides, have also been reported in the literature. The effects of air pollutants are dependent both on the concentration of the contaminant and the duration of the exposure. The term "injury," as opposed to damage, is commonly used to describe all plant responses to air contaminants and will be used in the context of this analysis. Air contaminants are thought to interact primarily with plant foliage,



which is considered to be the major pathway of exposure. For purposes of this analysis, it was assumed that 100 percent of each air contaminant of concern is accessible to the plants.

Injury to vegetation from exposure to various levels of air contaminants can be termed acute, physiological, or chronic. Acute injury occurs as a result of a short-term exposure to a high contaminant concentration and is typically manifested by visible injury symptoms ranging from chlorosis (discoloration) to necrosis (dead areas). Physiological or latent injury occurs as the result of a long-term exposure to contaminant concentrations below that which results in acute injury symptoms. Chronic injury results from repeated exposure to low concentrations over extended periods of time, often without any visible symptoms, but with some effect on the overall growth and productivity of the plant. In this assessment, 100 percent of the particular air pollutant in the ambient air was assumed to interact with the vegetation. This is a conservative approach.

The concentrations of the pollutants, duration of exposure and frequency of exposures influence the response of vegetation and wildlife to atmospheric pollutants. The pattern of pollutant exposure expected from the facility is that of a few episodes of relatively high ground-level concentration which occur during certain meteorological conditions interspersed with long periods of extremely low ground-level concentrations. If there are any effects of stack emissions on plants and animals they will be from the short-term, higher doses. A dose is the product of the concentration of the pollutant and duration of the exposure.

### 7.3.3.1 SO<sub>2</sub>

Sulfur is an essential plant nutrient usually taken up as sulfate ions by the roots from the soil solution. When sulfur dioxide in the atmosphere enters the foliage through pores in the leaves, it reacts with water in the leaf interior to form sulfite ions. Sulfite ions are highly toxic. They interact with enzymes, compete with normal metabolites, and interfere with a variety of cellular functions (Horsman and Wellburn, 1976). However, within the leaf, sulfite is oxidized to sulfate ions, which can then be used by the plant as a nutrient. Small amounts of sulfite may be oxidized before they prove harmful.

SO<sub>2</sub> gas at elevated levels has long been known to cause injury to plants. Acute SO<sub>2</sub> injury usually develops within a few hours or days of exposure, and symptoms include marginal, flecked, and/or intercostal necrotic areas that appear water-soaked and dullish green initially. This injury generally occurs to younger leaves. Chronic injury usually is evident by signs of chlorosis, bronzing, premature senescence, reduced growth, and possible tissue necrosis (EPA, 1982). Background levels of SO<sub>2</sub> in the Chassahowitzka NWA average 1.29 µg/m<sup>3</sup>, with a 24-hour maximum average concentration of 14.5 µg/m<sup>3</sup>. Observed SO<sub>2</sub> effect levels for several plant species and plant sensitivity groupings are presented in Tables 7-2 and 7-3, respectively.

Many studies have been conducted to determine the effects of high-concentration, short-term SO<sub>2</sub> exposure on natural community vegetation. Sensitive plants include ragweed, legumes, blackberry, southern pine, and red and black oak. These species are injured by exposure to 3-hour average SO<sub>2</sub> concentrations of 790 to 1,570 µg/m<sup>3</sup>. Intermediate plants include locust and sweetgum. These species are injured by exposure to 3-hour average SO<sub>2</sub> concentrations of 1,570 to 2,100 µg/m<sup>3</sup>. Resistant species (injured at concentrations above 2,100 µg/m<sup>3</sup> for 3 hours) include white oak and dogwood (EPA, 1982).

A study of native Floridian species (Woltz and Howe, 1981) demonstrated that cypress, slash pine, live oak, and mangrove exposed to 1,300 µg/m<sup>3</sup> SO<sub>2</sub> for 8 hours were not visibly damaged.

This finding support the levels cited by other researchers on the effects of SO<sub>2</sub> on vegetation. A corroborative study (McLaughlin and Lee, 1974) demonstrated that approximately 20 percent of a cross-section of plants ranging from sensitive to tolerant was visibly injured at 3-hour average SO<sub>2</sub> concentrations of 920 µg/m<sup>3</sup>.

Jack pine seedlings exposed to SO<sub>2</sub> concentrations of 470 to 520 µg/m<sup>3</sup> for 24 hours demonstrated inhibition of foliar lipid synthesis; however, this inhibition was reversible (Malhotra and Kahn, 1978). Black oak exposed to 1,310 µg/m<sup>3</sup> SO<sub>2</sub> for 24 hours a day for 1 week demonstrated a 48 percent reduction in photosynthesis (Carlson, 1979).

Two lichen species indigenous to Florida exhibited signs of SO<sub>2</sub> damage in the form of decreased biomass gain and photosynthetic rate as well as membrane leakage when exposed to concentrations of 200 to 400 µg/m<sup>3</sup> for 6 hours/week for 10 weeks (Hart et al., 1988).

The maximum 24-hour average SO<sub>2</sub> concentration that is predicted for the Project at the Class I area is 0.072 µg/m<sup>3</sup>. When added to the average background concentration of 1.29 µg/m<sup>3</sup>, total SO<sub>2</sub> impact is 1.36 µg/m<sup>3</sup>. When added to the maximum 24-hour average background concentration of 14.5 µg/m<sup>3</sup> at the NWA, the maximum worst-case total SO<sub>2</sub> concentration is 14.6 µg/m<sup>3</sup>, which is much lower than those known to cause damage to test species. The maximum 24-hour average SO<sub>2</sub> concentrations predicted for the Project at the Class I area are only 4 to 7 percent of those that caused damage to the most sensitive lichens. The modeled annual incremental increase in SO<sub>2</sub> adds slightly to background levels of this gas and poses only a minimal threat to area vegetation.

#### 7.3.3.2 PM<sub>10</sub>

Although information pertaining to the effects of particulate matter on plants is scarce, some research results are available. In a study conducted by Mandoli and Dubey (1988), ten species of native Indian plants were exposed to levels of particulate matter that ranged from 210 to 366

$\mu\text{g}/\text{m}^3$  for an 8-hour averaging period. Damage in the form of a higher leaf area/dry weight ratio was observed at varying degrees for most plants tested. Concentrations of particulate matter lower than  $163 \mu\text{g}/\text{m}^3$  did not appear to be injurious to the tested plants.

By comparison of these published toxicity values for particulate matter exposure with modeled concentrations, the possibility of plant damage in the Chassahowitzka NWA can be determined. The maximum  $\text{PM}_{10}$  concentrations predicted by the Project in the Class I area are 0.074 and  $0.037 \mu\text{g}/\text{m}^3$  for 8- and 24-hour averaging times, respectively (see Table 7-1). The 24-hour average background  $\text{PM}_{10}$  concentration reported for Chassahowitzka NWA is  $21.1 \mu\text{g}/\text{m}^3$ . The 8-hour average background was estimated by multiplying the 24-hour average concentration by three. This produced a conservative 8-hour average background concentration of  $63.3 \mu\text{g}/\text{m}^3$ . When added to the maximum 8-hour average  $\text{PM}_{10}$  concentrations of  $0.074 \mu\text{g}/\text{m}^3$  predicted by the Project in the NWA, the maximum total 8-hour average concentration of  $63.4 \mu\text{g}/\text{m}^3$  is well below the lower threshold value that reportedly affects plant foliage. As a result, no effects to vegetative AQRVs are expected from the Project's emissions.

#### 7.3.3.3 NO<sub>2</sub>

$\text{NO}_2$  can injure plant tissue with symptoms usually appearing as irregular white to brown collapsed lesions between the leaf veins and near the margins. Conversely, non-injurious levels of  $\text{NO}_2$  can be absorbed by plants, enzymatically transformed into ammonia, and incorporated into plant constituents such as amino acids (Matsumaru et al., 1979).

Plant damage can occur through either acute (short-term, high concentration) or chronic (long-term, relatively low concentration) exposure. For plants that have been determined to be more sensitive to  $\text{NO}_2$  exposure than others, acute (1, 4, 8 hours) exposure caused 5 percent predicted foliar injury at concentrations ranging from 3,800 to  $15,000 \mu\text{g}/\text{m}^3$  (Heck and Tingey, 1979). Chronic exposure of selected plants (some considered  $\text{NO}_2$ -sensitive) to  $\text{NO}_2$  concentrations of

2,000 to 4,000  $\mu\text{g}/\text{m}^3$  for 213 to 1,900 hours caused reductions in yield of up to 37 percent and some chlorosis (Zahn, 1975).

The 8-hour average  $\text{NO}_2$  concentration for the Project in the Class I area is predicted to be 0.42  $\mu\text{g}/\text{m}^3$ . This concentration is less than 0.01 percent of the levels that cause foliar injury in acute exposure scenarios. By comparison of published toxicity values for  $\text{NO}_2$  exposure to long-term (annual averaging time) modeled concentrations, the possibility of plant damage in the Class I areas can be examined for chronic exposure situations. For a chronic exposure, the maximum annual average  $\text{NO}_2$  concentration due to the Project in the Class I area is 0.0033  $\mu\text{g}/\text{m}^3$ . This value is less than 0.001 percent of the levels that caused minimal yield loss and chlorosis in plant tissue. Average and maximum background 24-hour average concentrations of  $\text{NO}_2$  reported in the Chassahowitzka NWA are 0.006 and 0.104  $\mu\text{g}/\text{m}^3$ , respectively.

Although it has been shown that simultaneous exposure to  $\text{SO}_2$  and  $\text{NO}_2$  results in synergistic plant injury (Ashenden and Williams, 1980), the magnitude of this response is generally only 3 to 4 times greater than either gas alone and usually occurs at unnaturally high levels of each gas. Therefore, the concentrations within the wilderness areas are still far below the levels that potentially cause plant injury for either acute or chronic exposure.

#### 7.3.3.4 CO

As with PM, information pertaining to the effects of CO on plants is scarce. The main effect of high concentrations of CO is the inhibition of cytochrome *c* oxidase, the terminal oxidase in the mitochondrial electron transfer chain. Inhibition of cytochrome *c* oxidase depletes the supply of ATP, the principal donor of free energy required for cell functions. However, this inhibition only occurs at extremely high concentrations of CO. Pollok et al. (1989) reported that acute exposure to CO: $\text{O}_2$  ratio of 25 (equivalent to an ambient CO concentration of  $6.85 \times 10^6 \mu\text{g}/\text{m}^3$ ) resulted in stomatal closure in the leaves of the sunflower (*Helianthus annuus*). Naik et al. (1992)

reported cytochrome *c* oxidase inhibition in corn, sorghum, millet, and Guinea grass at CO:O<sub>2</sub> ratios of 2.5 (equivalent to an ambient CO concentration of  $6.85 \times 10^5 \mu\text{g}/\text{m}^3$ ). These plants were considered the species most sensitive to CO-induced inhibition of cytochrome *c* oxidase.

By comparison of published effect values for CO exposure, the possibility of plant damage in the Class I areas can be determined. The maximum 1-hour average concentration due to the Project in the Class I area is  $0.34 \mu\text{g}/\text{m}^3$ , which is less than 0.001 percent of the minimum value that caused inhibition in laboratory studies.

#### 7.3.3.5 Sulfuric Acid Mist

Acidic precipitation or acid rain is coupled to SO<sub>2</sub> emissions mainly formed during the burning of fossil fuels. This pollutant is oxidized in the atmosphere and dissolves in rain forming sulfuric acid mist which falls as acidic precipitation (Ravera, 1989). Although concentration data are not available, sulfuric acid mist has been reported to yield necrotic spotting on the upper surfaces of leaves (Middleton et al, 1950).

No significant adverse effects on vegetation are expected from the Project's emissions because SO<sub>2</sub> concentrations, which lead directly to the formation of sulfuric acid mist concentrations, are predicted to be well below levels which have been documented as negatively affecting vegetation. During the last decade, much attention has been focused on acid rain. Acidic deposition is an ecosystem-level problem that affects vegetation because of some alterations of soil conditions such as increased leaching of essential base cations or elevated concentrations of aluminum in the soil water (Goldstein et al. 1985). Although effects of acid rain in eastern North America have been well published and publicized, detrimental effects of acid rain on Florida vegetation are lacking documentation.

### 7.3.3.6 Summary

In summary, the phytotoxic effects from the Peace River Station's emissions are minimal. It is important to note that the elements were conservatively modeled with the assumption that 100 percent was available for plant uptake. This is rarely the case in a natural ecosystem.

### 7.3.4 IMPACTS TO WILDLIFE

The major air quality risk to wildlife in the United States is from continuous exposure to pollutants above the National AAQS. This occurs in non-attainment areas, e.g., Los Angeles Basin. Risks to wildlife also may occur for wildlife living in the vicinity of an emission source that experiences frequent upsets or episodic conditions resulting from malfunctioning equipment, unique meteorological conditions, or startup operations (Newman and Schreiber, 1988). Under these conditions, chronic effects (e.g., particulate contamination) and acute effects (e.g., injury to health) have been observed (Newman, 1981).

A wide range of physiological and ecological effects to fauna has been reported for gaseous and particulate pollutants (Newman, 1981; Newman and Schreiber, 1988). The most severe of these effects have been observed at concentrations above the secondary ambient air quality standards. Physiological and behavioral effects have been observed in experimental animals at or below these standards. For impacts on wildlife, the lowest threshold values of SO<sub>2</sub>, NO<sub>2</sub>, and particulates which are reported to cause physiological changes are shown in Table 7-4. These values are up to orders of magnitude larger than maximum concentrations predicted for the Peace River Station for the Class I area. No effects on wildlife AQRVs from SO<sub>2</sub>, NO<sub>2</sub>, and particulates are expected. The proposed Project's contribution to cumulative impacts is negligible.

### 7.3.5 IMPACTS UPON VISIBILITY

#### 7.3.5.1 General

Visibility is an AQRV for the Chassahowitzka NWA. Visibility can take the form of plume blight for nearby areas, or regional haze for long distances (e.g., distances beyond 50 km). Because the Chassahowitzka NWA is more than 50 km from the Peace River Station, the change in visibility is analyzed as regional haze. Current regional haze guidelines characterize a change in visibility by either of the following methods:

1. Change in the visual range, defined as the greatest distance that a large dark object can be seen, or
2. Change in the light-extinction coefficient ( $b_{ext}$ ).

The  $b_{ext}$  is the attenuation of light per unit distance due to the scattering and absorption by gases and particles in the atmosphere. A change in the extinction coefficient produces a perceived visual change that is measured by a visibility index called the deciview. The deciview ( $dv$ ) is defined as:

$$dv = 10 \ln (1 + b_{exts} / b_{extb})$$

where:  $b_{exts}$  is the extinction coefficient calculated for the source, and  
 $b_{extb}$  is the background extinction coefficient

A similar index that simply quantifies the percent change in visibility due to the operation of a source is calculated as:

$$\Delta\% = (b_{exts} / b_{extb}) \times 100$$

#### 7.3.5.2 IWAQM Recommendations

The CALPUFF air modeling analysis followed the recommendations contained in the IWAQM Phase 2 Summary Report (EPA, 1998). A detailed description of the methods and assumptions



used in this is presented in Appendix C. Air quality impacts for the refined analyses were calculated as follows:

1. Obtain maximum 24-hour sulfate ( $\text{SO}_4$ ) and nitrate ( $\text{NO}_3$ ) impacts, in units of micrograms per cubic meter ( $\mu\text{g}/\text{m}^3$ ).

2. Convert the  $\text{SO}_4$  impact to ammonium sulfate ( $(\text{NH}_4)_2\text{SO}_4$ ) by the following formula:  

$$(\text{NH}_4)_2\text{SO}_4 (\mu\text{g}/\text{m}^3) = \text{SO}_4 (\mu\text{g}/\text{m}^3) \times \text{molecular weight } (\text{NH}_4)_2\text{SO}_4 / \text{molecular weight } \text{SO}_4$$

$$(\text{NH}_4)_2\text{SO}_4 (\mu\text{g}/\text{m}^3) = \text{SO}_4 (\mu\text{g}/\text{m}^3) \times 132/96$$

$$= \text{SO}_4 (\mu\text{g}/\text{m}^3) \times 1.375$$

3. Convert the  $\text{NO}_3$  impact to ammonium nitrate ( $\text{NH}_4\text{NO}_3$ ) by the following formula:  

$$\text{NH}_4\text{NO}_3 (\mu\text{g}/\text{m}^3) = \text{NO}_3 (\mu\text{g}/\text{m}^3) \times \text{molecular weight } \text{NH}_4\text{NO}_3 / \text{molecular weight } \text{NO}_3$$

$$\text{NH}_4\text{NO}_3 (\mu\text{g}/\text{m}^3) = \text{NO}_3 (\mu\text{g}/\text{m}^3) \times 80/62$$

$$= \text{NO}_3 (\mu\text{g}/\text{m}^3) \times 1.29$$

4. Compute  $b_{\text{exts}}$  (extinction coefficient calculated for the source) with the following formula:

$$b_{\text{exts}} = 3 \times \text{NH}_4\text{NO}_3 \times f(\text{RH}) + 3 \times (\text{NH}_4)_2\text{SO}_4 \times f(\text{RH}) + 3 \times \text{PM}_{10}$$

5. Compute  $b_{\text{extb}}$  (background extinction coefficient) using the background visual range (km) from the FLM with the following formula:

$$b_{\text{extb}} = 3.912 / \text{Visual range (km)}$$

6. Compute the change in extinction coefficients:

In terms of deciviews:

$$dv = 10 \ln (1 + b_{\text{exts}} / b_{\text{extb}})$$

In terms of percent change of visibility:

$$\Delta\% = (b_{\text{exts}} / b_{\text{extb}}) \times 100$$

Based on the predicted  $\text{SO}_4$ ,  $\text{NO}_3$ , and  $\text{PM}_{10}$  concentrations, the Project's emissions are compared to a 5 percent change in light extinction of the background levels. This is equivalent to a change in deciview of 0.5.

### 7.3.5.3 Background Visual Ranges And Relative Humidity Factors

The background visual range is based on data representative of the top 20-percentile of visual range data measured at Chassahowitzka NWA. The background visual range for the Chassahowitzka NWA is 65 km and was provided by the FLM. The average relative humidity

factor for each day during which the highest concentrations were predicted was computed by averaging the hourly relative humidity factor based on the hourly relative humidity for the 24-hour period. This factor was estimated by using data presented in the Federal Land Managers' Air Quality Related Values Workgroup (FLAG), Draft Phase I Report (October 1999).

#### 7.3.5.4 Regional Haze Analysis

The results of the Phase 2 refined analysis for regional haze are summarized in Tables 7-5 through 7-7. As shown in Table 7-5, the maximum pollutant impacts were predicted to occur on August 16, 1990 (Julian Day 228) for SO<sub>4</sub>, July 4, 1990 (Julian Day 185) for NO<sub>3</sub>, and May 16, 1990 (Julian Day 136) for PM<sub>10</sub>. The calculated average relative humidity factors for these days are presented in Table 7-6. The maximum changes in visibility due to the Project for these days are summarized in Table 7-7. As shown in Table 7-7, the maximum change in visibility on July 4 is estimated to be 2.2 percent or 0.22 deciviews. This impact is below the FLM's screening criteria of 5 percent or 0.5 deciview change. As a result, this indicates that the Peace River Station would not have an adverse impact on the existing regional haze at the PSD Class I area of the Chassahowitzka NWA.

Table 7-1. Maximum Pollutant Concentrations Due to the Peace River Station Predicted at the PSD Class I Area of the Chassahowitzka National Wilderness Area

Pollutant	Maximum Concentration <sup>a</sup> ( $\mu\text{g}/\text{m}^3$ )				
	Annual	24-Hour	8-Hour	3-Hour	1-Hour
Sulfur Dioxide ( $\text{SO}_2$ )	0.0041	0.072	0.15	0.26	0.33
Nitrogen Dioxide ( $\text{NO}_2$ )	0.0033	0.16	0.42	0.67	0.84
Particulates ( $\text{PM}_{10}$ )	0.0021	0.037	0.074	0.12	0.15
Carbon Monoxide (CO)	0.0060	0.089	0.16	0.27	0.34

<sup>a</sup> Based on maximum concentrations using the CALPUFF model.

Table 7-2. SO<sub>2</sub> Effects Levels for Various Plant Species

Plant Species	Observed Effect Level ( $\mu\text{g}/\text{m}^3$ )	Exposure (Time)	Reference
Sensitive to tolerant	920 (20 percent displayed visible injury)	3 hours	McLaughlin and Lee, 1974
Lichens	200-400	6 hr/wk for 10 weeks	Hart <i>et al.</i> , 1988
Cypress, slash pine, live oak, mangrove	1,300	8 hours	Woltz and Howe, 1981
Jack pine seedlings	470-520	24 hours	Malhotra and Kahn, 1978
Black oak	1,310	Continuously for 1 week	Carlson, 1979

Table 7-3. Sensitivity Groupings of Vegetation Based on Visible Injury at Different SO<sub>2</sub> Exposures<sup>a</sup>

Sensitivity Grouping	SO <sub>2</sub> Concentration		Plants
	1-Hour	3-Hour	
Sensitive	1,310 - 2,620 $\mu\text{G}/\text{m}^3$ (0.5 - 1.0 ppm)	790 - 1,570 $\mu\text{G}/\text{m}^3$ (0.3 - 0.6 ppm)	Ragweeds Legumes Blackberry Southern pines Red and black oaks White ash Sumacs
Intermediate	2,620 - 5,240 $\mu\text{G}/\text{m}^3$ (1.0 - 2.0 ppm)	1,570 - 2,100 $\mu\text{G}/\text{m}^3$ (0.6 - 0.8 ppm)	Maples Locust Sweetgum Cherry Elms Tuliptree Many crop and garden species
Resistant	>5,240 $\mu\text{G}/\text{m}^3$ (>2.0 ppm)	>2,100 $\mu\text{G}/\text{m}^3$ (>0.8 ppm)	White oaks Potato Upland cotton Corn Dogwood Peach

<sup>a</sup> Based on observations over a 20-year period of visible injury occurring on over 120 species growing in the vicinities of coal-fired power plants in the southeastern United States.

Source: EPA, 1982a.

Table 7-4. Examples of Reported Effects of Air Pollutants at Concentrations Below National Secondary Ambient Air Quality Standards

Pollutant	Reported Effect	Concentration ( $\mu\text{g}/\text{m}^3$ )	Exposure
Sulfur Dioxide <sup>a</sup>	Respiratory stress in guinea pigs	427 to 854	1 hour
	Respiratory stress in rats	267	7 hours/day; 5 day/week for 10 weeks
	Decreased abundance in deer mice	13 to 157	continually for 5 months
Nitrogen Dioxide <sup>b,c</sup>	Respiratory stress in mice	1,917	3 hours
	Respiratory stress in guinea pigs	96 to 958	8 hours/day for 122 days
Particulates <sup>a</sup>	Respiratory stress, reduced respiratory disease defenses	120 $\text{PbO}_3$	continually for 2 months
	Decreased respiratory disease defenses in rats, same with hamsters	100 $\text{NiCl}_2$	2 hours

Source: <sup>a</sup>Newman and Schreiber, 1988.

<sup>b</sup>Gardner and Graham, 1976.

<sup>c</sup>Trzeciak et al., 1977.

Table 7-5. Maximum Pollutant Concentrations Predicted for the Peace River Station  
at the Chassahowitzka PSD Class I Area

Pollutant	Maximum Predicted Concentrations <sup>a</sup> (ug/m3)		
	May 16 (136)	July 4 (185)	August 16 (228)
SO <sub>4</sub>	0.0197	0.0164	0.0430 <sup>b</sup>
NO <sub>3</sub>	0.0281	0.0985 <sup>b</sup>	0.0411
PM <sub>10</sub>	0.0366 <sup>b</sup>	0.0268	0.0362

<sup>a</sup> Predicted with CALPUFF model in the refined mode (Julian Day in parentheses)

<sup>b</sup> Highest concentration predicted for specific pollutant. Maximum concentrations for for SO<sub>4</sub> and NO<sub>3</sub> predicted for 100 % load at 32 °F; for PM<sub>10</sub>, maximum concentration predicted for 50% load, 95 °F.

Table 7-6. Computed Daily Average RH Factors for Days of Maximum Impacts Predicted for the Peace River Station at the PSD Class I Area of the Chassahowitzka NWA

Hour Ending	May 16 (136) <sup>a</sup>		July 4 (185) <sup>a</sup>		August 16 (228) <sup>a</sup>	
	RH(%)	f(RH)	RH(%)	f(RH)	RH(%)	f(RH)
0	87	3.8	90	4.7	87	3.8
1	87	3.8	82	3.0	90	4.7
2	90	4.7	85	3.4	94	8.4
3	94	8.4	87	3.8	94	8.4
4	97	15.1	90	4.7	94	8.4
5	93	7.0	87	3.8	94	8.4
6	93	7.0	93	7.0	94	8.4
7	90	4.7	85	3.4	88	4.0
8	82	3.0	74	2.1	82	3.0
9	69	1.9	69	1.9	77	2.4
10	57	1.3	67	1.7	68	1.8
11	52	1.3	61	1.5	59	1.4
12	47	1.2	55	1.3	52	1.3
13	42	1.1	52	1.3	52	1.3
14	37	1.1	42	1.1	49	1.2
15	37	1.1	46	1.2	49	1.2
16	39	1.1	52	1.3	47	1.2
17	42	1.1	61	1.5	50	1.2
18	52	1.3	67	1.7	74	2.1
19	55	1.3	72	2.0	82	3.0
20	56	1.3	72	2.0	74	2.1
21	62	1.5	74	2.1	77	2.4
22	67	1.7	79	2.6	85	3.4
23	76	2.3	82	3.0	85	3.4
Average		3.25		2.59		3.62

Note: RH = relative humidity; f(RH) = relative humidity factor

<sup>a</sup> Hourly relative humidity data for 1990 from the National Weather Service station at the Tampa International Airport in Tampa, Florida. Julian day in parenthesis.



Table 7-7. Summary of the Refined Regional Haze Analyses for the Peace River Station's Impacts Predicted at the PSD Class I Area of the Chassahowitzka NWA

Parameter	Units	Days of Maximum Concentrations Predicted for the Project		
		May 16 (136)	July 4 (185)	August 16 (228)
<b><u>Maximum Predicted Concentration</u></b>				
SO <sub>4</sub>	ug/m <sup>3</sup>	0.0197	0.0164	0.0430
NO <sub>3</sub>		0.0281	0.0985	0.0411
PM10		0.0366	0.0268	0.0362
<b><u>Computed Concentrations</u></b>				
(NH <sub>4</sub> ) <sub>2</sub> SO <sub>4</sub>	ug/m <sup>3</sup>	0.0271	0.0225	0.0591
NH <sub>4</sub> NO <sub>3</sub>		0.0362	0.1270	0.0530
Average Relative Humidity Factor <sup>a</sup>		3.25	2.59	3.62
Background Visual Range (Vr) <sup>b</sup>		65	65	65
Background Extinction Coefficient (bext)	km <sup>-1</sup>	0.0602	0.0602	0.0602
<b><u>Source Extinction Coefficients (bexts)</u></b>				
(NH <sub>4</sub> ) <sub>2</sub> SO <sub>4</sub>	km <sup>-1</sup>	0.000264	0.000175	0.000642
NH <sub>4</sub> NO <sub>3</sub>		0.000354	0.000986	0.000575
PM10		0.000110	0.000080	0.000109
Total bexts	km <sup>-1</sup>	0.000728	0.001241	0.001326
Deciview Change		0.120	0.204	0.218
Percent Change (%)		1.20	2.04	2.18
Allowable Criteria (%)		5.0	5.0	5.0

<sup>a</sup> Computed from relative humidity data measured in 1990 at the National Weather Service station at the Tampa International Airport, Florida

<sup>b</sup> Provided by U.S. Fish and Wildlife Service

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**APPENDIX A**

**EXPECTED PERFORMANCE AND EMISSION INFORMATION  
ON GE FRAME 7FA COMBUSTION TURBINE**

**(Note: SO<sub>2</sub> emissions based on 2 gr/100 cf of sulfur to account for  
odorant (mercaptans) in pipeline gas.)**

Table A-1. Design Information and Stack Parameters  
General Electric Frame 7FA Simple Cycle Unit, Dry Low NOx Combustor, Natural Gas, 100 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
<b>Combustion Turbine Performance</b>				
Evaporative cooler status/ efficiency (%)	Off	On	On	On
Ambient Relative Humidity (%)	80	60	75	95
Gross power output (MW)	183.53	174.41	162.46	155.72
Gross heat rate (Btu/kWh, LHV)	9,143	9,254	9,448	9,569
(Btu/kWh, HHV)	10,149	10,272	10,488	10,621
Heat Input (MMBtu/hr, LHV)- calculated	1,678	1,614	1,535	1,490
- provided	1,678	1,614	1,535	1,490
(MMBtu/hr, HHV) - calculated	1,863	1,792	1,704	1,654
(HHV/LHV)	1.11	1.11	1.11	1.11
Fuel heating value (Btu/lb, LHV)	21,511	21,511	21,511	21,511
(Btu/lb, HHV)	23,877	23,877	23,877	23,877
(HHV/LHV)	1.11	1.11	1.11	1.11
<b>CT Exhaust Flow</b>				
Mass Flow (lb/hr)	3,701,000	3,557,000	3,396,000	3,306,000
Temperature (°F)	1,096	1,117	1,135	1,144
Moisture (% Vol.)	7.93	8.65	9.93	10.71
Oxygen (% Vol.)	12.60	12.46	12.26	12.13
Molecular Weight - calculated	28.44	28.36	28.21	28.13
- provided	28.44	28.36	28.21	28.13
<b>Volume Flow (acfm) = [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F) + 460°F)] / [Molecular weight x 2116.8] / 60 min/hr</b>				
Mass flow (lb/hr)	3,701,000	3,557,000	3,396,000	3,306,000
Temperature (°F)	1,096	1,117	1,135	1,144
Molecular weight	28.44	28.36	28.21	28.13
Volume flow (acfm)- calculated	2,463,574	2,406,262	2,335,408	2,293,500
- provided	2,496,900	2,412,600	2,341,500	2,299,400
	1.014	1.003	1.003	1.003
<b>Fuel Usage</b>				
<b>Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu (Fuel Heat Content, Btu/lb (LHV))</b>				
Heat input (MMBtu/hr, LHV)	1,678	1,614	1,535	1,490
Heat content (Btu/lb, LHV)	21,511	21,511	21,511	21,511
Fuel usage (lb/hr)- calculated	78,007	75,031	71,359	69,267
- provided	78,000	75,000	71,400	69,300
Heat content (Btu/cf, LHV)- assumed	920	920	920	920
Fuel density (lb/ft <sup>3</sup> )	0.0428	0.0428	0.0428	0.0428
Fuel usage (cf/hr)- calculated	1,823,913	1,754,348	1,668,478	1,619,565
(cf/yr)	6,183,070,000	5,947,240,000	5,656,140,000	5,490,330,000
<b>Stack and Exit Gas Conditions</b>				
Stack height (ft)	60	60	60	60
Diameter (ft)	21.0	21.0	21.0	21.0
<b>Velocity (ft/sec) = Volume flow (acfm) / [((diameter)<sup>2</sup>/4) x 3.14159] / 60 sec/min</b>				
Volume flow (acfm)- from CT	2,496,900	2,406,262	2,335,408	2,293,500
Temperature (°F) (-20 oF from CT exhaust)	1,076	1,097	1,115	1,124
Exit gas volume flow (acfm)	2,464,806	2,375,745	2,306,123	2,264,903
Diameter (ft)	21.0	21.0	21.0	21.0
Velocity (ft/sec)- calculated	118.6	115.8	112.4	110.4
Velocity (ft/sec)- provided	118.9	116.1	112.7	110.6
Velocity (m/sec)- from calculated value	36.15	35.29	34.25	33.64

Source: General Electric, 1999; Decker Energy International, 2000.

Note: Universal gas constant = 1,545 ft-lb(force)/°R; atmospheric pressure = 2,116.8 lb(force)/ft<sup>2</sup>

Table A-2. Maximum Emissions for Criteria and Other Regulated Pollutants  
General Electric Frame 7FA Simple Cycle Unit, Dry Low NOx Combustor, Natural Gas, 100 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	3,390	3,390	3,390	3,390
Particulate from CT= Emission rate (lb/hr) from CT manufacturer (dry filterables)				
Basis, lb/hr - provided (a) (b)	11.0	11.0	11.0	11.0
(TPY)	18.6	18.6	18.6	18.6
Sulfur Dioxide (lb/hr) = Natural gas (cf/hr) x sulfur content (gr/100 cf) x 1 lb/7000 gr x (lb SO <sub>2</sub> /lb S) /100				
Fuel use (cf/hr)	1,823,913	1,754,348	1,668,478	1,619,565
Sulfur content (grains/ 100 cf) - assumed (b)	2	2	2	2
lb SO <sub>2</sub> /lb S (64/32)	2	2	2	2
Emission rate (lb/hr)- calculated	10.4	10.0	9.5	9.3
(lb/hr)- provided (0.5 gr/100 cf)	2.8	2.7	2.6	2.5
(TPY)	17.7	17.0	16.2	15.7
[Ratio lb/hr provided/calculated]	0.269	0.269	0.273	0.270
Nitrogen Oxides (lb/hr) = NOx(ppm) x {[20.9 x (1 - Moisture%/100)] - Oxygen(%)} x 2116.8 x Volume flow (acfm) x 46 (mole. wt NOx) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]				
Basis, ppmvd @ 15% O <sub>2</sub> (a) (b)	10.0	10.0	10.0	10.0
Moisture (%)	7.93	8.65	9.93	10.71
Oxygen (%)	12.60	12.46	12.26	12.13
Volume Flow (acfm)	2,496,900	2,412,600	2,341,500	2,299,400
Temperature (°F)	1,096	1,117	1,135	1,144
Emission rate (lb/hr)- calculated	68.2	65.0	61.7	60.0
(lb/hr)- provided	71.9	69.3	65.7	63.9
(TPY)	121.9	117.4	111.4	108.4
[Ratio lb/hr provided/calculated]	1.054	1.066	1.065	1.066
Carbon Monoxide (lb/hr) = CO(ppm) x {[20.9 x (1 - Moisture%/100)] - Oxygen(%)} x 2116.8 lb/ft <sup>2</sup> x Volume flow (acfm) x 28 (mole. wt CO) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]				
Basis, ppmvd- calculated	10.0	10.0	10.0	10.0
Basis, ppmvd @ 15% O <sub>2</sub> - calculated	8.2	8.1	8.1	8.1
- provided (a) (b)	8.2	8.1	8.1	8.1
Moisture (%)	7.93	8.65	9.93	10.71
Oxygen (%)	12.60	12.46	12.26	12.13
Volume Flow (acfm)	2,496,900	2,412,600	2,341,500	2,299,400
Temperature (°F)	1,096	1,117	1,135	1,144
Emission rate (lb/hr)- calculated from given ppmvd	34.2	32.1	30.5	29.6
(lb/hr)- provided	35.9	34.3	32.4	31.4
(TPY)	60.8	58.1	54.9	53.2
[Ratio lb/hr provided/calculated]	1.050	1.069	1.064	1.061
VOCs (lb/hr) = VOC(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft <sup>2</sup> x Volume flow (acfm) x 16 (mole. wt as methane) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]				
Basis, ppmvd (as CH <sub>4</sub> )- calculated	2.0	2.0	2.2	2.2
Basis, ppmvd @ 15% O <sub>2</sub> - calculated	1.6	1.6	1.8	1.8
- provided (a) (b)	1.6	1.6	1.8	1.8
Moisture (%)	7.93	8.65	9.93	10.71
Oxygen (%)	12.60	12.46	12.26	12.13
Volume Flow (acfm)	2,496,900	2,412,600	2,341,500	2,299,400
Temperature (°F)	1,096	1,117	1,135	1,144
Emission rate (lb/hr)- calculated	3.8	3.7	3.8	3.7
(lb/hr)- provided	4.2	4.1	3.9	3.8
(TPY)	7.1	6.9	6.6	6.4
[Ratio lb/hr provided/calculated]	1.087	1.105	1.038	1.032
Lead (lb/hr) = NA				
Emission Rate Basis	NA	NA	NA	NA
Emission rate (lb/hr)	NA	NA	NA	NA
(TPY)	NA	NA	NA	NA
Mercury (lb/hr) = Basis (lb/10 <sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>13</sup> Btu				
Basis, lb/10 <sup>13</sup> Btu (c)	8.00E-04	8.00E-04	8.00E-04	8.00E-04
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	1.49E-06	1.43E-06	1.36E-06	1.32E-06
(TPY)	2.53E-06	2.43E-06	2.31E-06	2.24E-06
Sulfuric Acid Mist = SO <sub>2</sub> emission rate (lb/hr) x conversion rate of SO <sub>2</sub> to H <sub>2</sub> SO <sub>4</sub> (%) x MW H <sub>2</sub> SO <sub>4</sub> / MW SO <sub>2</sub> (98/64)				
SO <sub>2</sub> emission rate (lb/hr)	10.4	10.0	9.5	9.3
lb H <sub>2</sub> SO <sub>4</sub> / lb SO <sub>2</sub> (98/64)	1.53	1.53	1.53	1.53
Conversion to H <sub>2</sub> SO <sub>4</sub> (%) (b)	15	15	15	15
Emission Rate (lb/hr)	2.39	2.30	2.19	2.13
(TPY)	4.06	3.90	3.71	3.60

Source: (a) General Electric 1999; (b) Decker Energy International, 2000; (c) EPRI, 1994  
Note: ppmvd = parts per million, volume dry; O<sub>2</sub> = oxygen.

Table A-3. Maximum Emissions for Other Regulated PSD Pollutants  
General Electric Frame 7FA Simple Cycle Unit, Dry Low NOx Combustor, Natural Gas, 100 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	3,390	3,390	3,390	3,390
2,3,7,8 TCDD Equivalents (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a) , lb/10 <sup>12</sup> Btu	1.20E-06	1.20E-06	1.20E-06	1.20E-06
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	2.24E-09	2.15E-09	2.04E-09	1.98E-09
(TPY)	3.79E-09	3.64E-09	3.47E-09	3.36E-09
Beryllium (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a) , lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Fluoride (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis, lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00

Source: Electric Power Research Institute (EPRI), Electric Utility Trace Substances Report, 1994 (Table B-12).  
Emission factors for metals are questionable and not used.

Note: No emission factors for hydrogen chloride (HCl) from natural gas-firing.

Table A-4. Maximum Emissions for Hazardous Air Pollutants  
General Electric Frame 7FA Simple Cycle Unit, Dry Low NOx Combustor, Natural Gas, 100 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	3,390	3,390	3,390	3,390
Antimony (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Benzene (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	0.8	0.8	0.8	0.8
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	1.49E-03	1.43E-03	1.36E-03	1.32E-03
(TPY)	2.53E-03	2.43E-03	2.31E-03	2.24E-03
Cadmium (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Chromium (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Formaldehyde (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	34	34	34	34
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	6.33E-02	6.09E-02	5.79E-02	5.62E-02
(TPY)	1.07E-01	1.03E-01	9.82E-02	9.53E-02
Cobalt (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Manganese (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Nickel (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Phosphorous (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (b), lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Selenium (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Toluene (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	10	10	10	10
Heat Input Rate (MMBtu/hr)	1,863	1,792	1,704	1,654
Emission Rate (lb/hr)	1.86E-02	1.79E-02	1.70E-02	1.65E-02
(TPY)	3.16E-02	3.04E-02	2.89E-02	2.80E-02

Source: Electric Power Research Institute (EPRI), Electric Utility Trace Substances Report, 1994 (Table B-12).  
Emission factors for metals are questionable and not used.



Table A-5. Design Information and Stack Parameters  
General Electric Frame 7 FA, Simple Cycle, Dry Low NOx Combustor, Natural Gas, 75 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
<b>Combustion Turbine Performance</b>				
Evaporative cooler status/ efficiency (%)	Off	Off	Off	Off
Ambient Relative Humidity (%)	80	60	87	55
Gross power output (MW)	137.66	126.23	120.69	110.63
Gross heat rate (Btu/kWh, LHV)	10,046	10,346	10,382	10,676
(Btu/kWh, HHV)	11,152	11,484	11,524	11,850
Heat Input (MMBtu/hr, LHV)- calculated	1,383	1,306	1,253	1,181
- provided	1,383	1,306	1,253	1,181
(MMBtu/hr, HHV) - calculated	1,535	1,450	1,391	1,311
(HHV/LHV)	1.11	1.11	1.11	1.11
Fuel heating value (Btu/lb, LHV)	21,511	21,511	21,511	21,511
(Btu/lb, HHV)	23,877	23,877	23,877	23,877
(HHV/LHV)	1.11	1.11	1.11	1.11
<b>CT Exhaust Flow</b>				
Mass Flow (lb/hr)	2,950,000	2,817,000	2,740,000	2,653,000
Temperature (°F)	1,184	1,199	1,200	1,200
Moisture (% Vol.)	8.18	8.60	9.94	10.22
Oxygen (% Vol.)	12.33	12.33	12.17	12.31
Molecular Weight - calculated	28.42	28.37	28.22	28.18
- provided	28.42	28.37	28.22	28.18
<b>Volume Flow (acfm) = [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F) + 460°F)] / [Molecular weight x 2116.8] / 60 min/hr</b>				
Mass flow (lb/hr)	2,950,000	2,817,000	2,740,000	2,653,000
Temperature (°F)	1,184	1,199	1,200	1,200
Molecular weight	28.42	28.37	28.22	28.18
Volume flow (acfm)- calculated	2,075,685	2,003,743	1,960,901	1,901,303
- provided	2,081,100	2,009,300	1,966,100	1,906,500
	1.003	1.003	1.003	1.003
<b>Fuel Usage</b>				
<b>Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu (Fuel Heat Content, Btu/lb (LHV))</b>				
Heat input (MMBtu/hr, LHV)	1,383	1,306	1,253	1,181
Heat content (Btu/lb, LHV)	21,511	21,511	21,511	21,511
Fuel usage (lb/hr)- calculated	64,293	60,713	58,249	54,902
- provided	64,300	60,700	58,200	54,900
Heat content (Btu/cf, LHV)	920	920	920	920
Fuel density (lb/ft <sup>3</sup> )	0.0428	0.0428	0.0428	0.0428
Fuel usage (cf/hr)- calculated	1,503,261	1,419,565	1,361,957	1,283,696
<b>Stack and Exit Gas Conditions</b>				
Stack height (ft)	60	60	60	60
Diameter (ft)	21.0	21.0	21.0	21.0
<b>Velocity (ft/sec) = Volume flow (acfm) / (((diameter)<sup>2</sup> / 4) x 3.14159) / 60 sec/min</b>				
Volume flow (acfm)- from CT	2,081,100	2,009,300	1,966,100	1,906,500
Temperature (°F) (-20 oF from CT exhaust)	1,164	1,179	1,180	1,180
Exit gas volume flow (acfm)	2,055,782	1,985,077	1,942,412	1,883,530
Diameter (ft)	21.0	21.0	21.0	21.0
Velocity (ft/sec)- calculated	100.1	96.7	94.6	91.7
Velocity (ft/sec)- provided	100.1	96.7	94.6	91.7
Velocity (m/sec)- from calculated value	30.52	29.47	28.84	27.96

Source: General Electric, 1999; Decker Energy International, 2000.

Note: Universal gas constant = 1,545 ft-lb(force)°R; atmospheric pressure = 2,116.8 lb(force)/ft<sup>2</sup>

Table A-6. Maximum Emissions for Criteria and Other Regulated Pollutants  
General Electric Frame 7 FA, Simple Cycle, Dry Low NOx Combustor, Natural Gas, 75 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	3,390	3,390	3,390	3,390
Particulate from CT = Emission rate (lb/hr) from CT manufacturer (dry filterables)				
Basis, lb/hr - provided (a) (b)	11.0	11.0	11.0	11.0
(TPY)	18.6	18.6	18.6	18.6
Sulfur Dioxide (lb/hr) = Natural gas (cf/hr) x sulfur content (gr/100 cf) x 1 lb/7000 gr x (lb SO <sub>2</sub> /lb S)/100				
Fuel use (cf/hr)	1,503,261	1,419,565	1,361,957	1,283,696
Sulfur content (grains/100 cf) - assumed (b)	2	2	2	2
lb SO <sub>2</sub> /lb S (64/32)	2	2	2	2
Emission rate (lb/hr) - calculated	8.6	8.1	7.8	7.3
(lb/hr) - provided (0.5 gr/100 cf)	2.30	2.20	2.10	2.00
(TPY)	14.6	13.7	13.2	12.4
[Ratio lb/hr provided/calculated]	0.268	0.271	0.270	0.273
Nitrogen Oxides (lb/hr) = NOx(ppm) x [(20.9 x (1 - Moisture(%)/100)) - Oxygen(%)] x 2116.8 x Volume flow (acfm) x 46 (mole. wtg NOx) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]				
Basis, ppmvd @15% O <sub>2</sub> (a) (b)	10.0	10.0	10.0	10.0
Moisture (%)	8.18	8.60	9.94	10.22
Oxygen (%)	12.33	12.33	12.17	12.31
Volume Flow (acfm)	2,081,100	2,009,300	1,966,100	1,906,500
Temperature (°F)	1,184	1,199	1,200	1,200
Emission rate (lb/hr) - calculated	55.6	52.5	50.5	47.5
(lb/hr) - provided	59.3	55.9	53.7	50.6
(TPY)	100.5	94.8	91.1	85.8
[Ratio lb/hr provided/calculated]	1.066	1.065	1.065	1.066
Carbon Monoxide (lb/hr) = CO(ppm) x [(20.9 x (1 - Moisture(%)/100)) - Oxygen(%)] x 2116.8 lb/ft <sup>2</sup> x Volume flow (acfm) x 28 (mole. wtg CO) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]				
Basis, ppmvd - calculated	10.0	10.0	10.0	10.0
Basis, ppmvd @ 15% O <sub>2</sub> - calculated	7.9	8.0	8.0	8.2
- provided (a) (b)	7.9	8.0	8.0	8.2
Moisture (%)	8.18	8.60	9.94	10.22
Oxygen (%)	12.33	12.33	12.17	12.31
Volume Flow (acfm)	2,081,100	2,009,300	1,966,100	1,906,500
Temperature (°F)	1,184	1,199	1,200	1,200
Emission rate (lb/hr) - calculated from given ppmvd	26.7	25.6	24.6	23.8
(lb/hr) - provided	28.5	27.2	26.2	25.3
(TPY)	48.4	46.1	44.4	42.9
[Ratio lb/hr provided/calculated]	1.069	1.063	1.066	1.065
VOCs (lb/hr) = VOC(ppm) x [1 - Moisture(%)/100] x 2116.8 lb/ft <sup>2</sup> x Volume flow (acfm) x 16 (mole. wtg as methane) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]				
Basis, ppmvd (as CH <sub>4</sub> ) - calculated	2.1	2.0	2.0	2.1
Basis, ppmvd @ 15% O <sub>2</sub> - calculated	1.6	1.6	1.6	1.8
- provided (a) (b)	1.6	1.6	1.6	1.8
Moisture (%)	8.18	8.60	9.94	10.22
Oxygen (%)	12.33	12.33	12.17	12.31
Volume Flow (acfm)	2,081,100	2,009,300	1,966,100	1,906,500
Temperature (°F)	1,184	1,199	1,200	1,200
Emission rate (lb/hr) - calculated	3.1	3.0	2.8	2.9
(lb/hr) - provided	3.4	3.2	3.1	3.1
(TPY)	5.7	5.5	5.3	5.3
[Ratio lb/hr provided/calculated]	1.076	1.094	1.091	1.071
Lead (lb/hr) = NA				
Emission Rate Basis	NA	NA	NA	NA
Emission rate (lb/hr)	NA	NA	NA	NA
(TPY)	NA	NA	NA	NA
Mercury (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis, lb/10 <sup>12</sup> Btu (c)	8.00E-04	8.00E-04	8.00E-04	8.00E-04
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	1.23E-06	1.16E-06	1.11E-06	1.05E-06
(TPY)	2.08E-06	1.97E-06	1.89E-06	1.78E-06
Sulfuric Acid Mist = SO <sub>2</sub> emission rate (lb/hr) x conversion rate of SO <sub>2</sub> to H <sub>2</sub> SO <sub>4</sub> (%) x MW H <sub>2</sub> SO <sub>4</sub> /MW SO <sub>2</sub> (98/64)				
SO <sub>2</sub> emission rate (lb/hr)	8.6	8.1	7.8	7.3
lb H <sub>2</sub> SO <sub>4</sub> /lb SO <sub>2</sub> (98/64)	1.53	1.53	1.53	1.53
Conversion to H <sub>2</sub> SO <sub>4</sub> (%) (b)	15	15	15	15
Emission Rate (lb/hr)	1.97	1.86	1.79	1.68
(TPY)	3.34	3.16	3.03	2.86

Source: (a) General Electric 1999; (b) Decker Energy International, 2000; (c) EPRI 1994  
Note: ppmvd = parts per million, volume dry; O<sub>2</sub> = oxygen.

Table A-7. Maximum Emissions for Other Regulated PSD Pollutants  
General Electric Frame 7 FA, Simple Cycle, Dry Low NOx Combustor, Natural Gas, 75 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	3,390	3,390	3,390	3,390
2,3,7,8 TCDD Equivalents (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a) , lb/10 <sup>12</sup> Btu	1.20E-06	1.20E-06	1.20E-06	1.20E-06
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	1.84E-09	1.74E-09	1.67E-09	1.57E-09
(TPY)	3.12E-09	2.95E-09	2.83E-09	2.67E-09
Beryllium (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a) , lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Fluoride (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis, lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00

Source: Electric Power Research Institute (EPRI), Electric Utility Trace Substances Report, 1994 (Table B-12).  
Emission factors for metals are questionable and not used.

Note: No emission factors for hydrogen chloride (HCl) from natural gas-firing.

Table A-8. Maximum Emissions for Hazardous Air Pollutants  
General Electric Frame 7 FA, Simple Cycle, Dry Low NOx Combustor, Natural Gas, 75 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	3,390	3,390	3,390	3,390
Antimony (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Benzene (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0.8	0.8	0.8	0.8
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	1.23E-03	1.16E-03	1.11E-03	1.05E-03
(TPY)	2.08E-03	1.97E-03	1.89E-03	1.78E-03
Cadmium (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Chromium (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Formaldehyde (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	34	34	34	34
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	5.22E-02	4.93E-02	4.73E-02	4.46E-02
(TPY)	8.85E-02	8.35E-02	8.02E-02	7.55E-02
Cobalt (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Manganese (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Nickel (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Phosphorous (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (b), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Selenium (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Toluene (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	10	10	10	10
Heat Input Rate (MMBtu/hr)	1,535	1,450	1,391	1,311
Emission Rate (lb/hr)	1.54E-02	1.45E-02	1.39E-02	1.31E-02
(TPY)	2.60E-02	2.46E-02	2.36E-02	2.22E-02

Source: Electric Power Research Institute (EPRI), Electric Utility Trace Substances Report, 1994 (Table B-12).  
Emission factors for metals are questionable and not used.

Table A-9. Design Information and Stack Parameters  
General Electric Frame 7FA, Simple Cycle, Dry Low NO<sub>x</sub> Combustor, Natural Gas, 50 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
<b>Combustion Turbine Performance</b>				
Evaporative cooler status/ efficiency (%)	Off	Off	Off	Off
Ambient Relative Humidity (%)	80	60	87	55
Gross power output (MW)	91.78	85.49	80.46	73.76
Gross heat rate (Btu/kWh, LHV)	11,386	11,487	11,758	12,175
(Btu/kWh, HHV)	12,638	12,751	13,051	13,515
Heat Input (MMBtu/hr, LHV)- calculated	1,045	982	946	898
- provided	1,045	982	946	898
(MMBtu/hr, HHV) - calculated	1,160	1,090	1,050	997
(HHV/LHV)	1.11	1.11	1.11	1.11
Fuel heating value (Btu/lb, LHV)	21,511	21,511	21,511	21,511
(Btu/lb, HHV)	23,877	23,877	23,877	23,877
(HHV/LHV)	1.11	1.11	1.11	1.11
<b>CT Exhaust Flow</b>				
Mass Flow (lb/hr)	2,586,000	2,570,000	2,515,000	2,452,000
Temperature (°F)	1,096	1,068	1,069	1,072
Moisture (% Vol.)	7.14	7.28	8.64	8.97
Oxygen (% Vol.)	13.49	13.79	13.61	13.70
Molecular Weight - calculated	28.49	28.46	28.30	28.26
- provided	28.49	28.46	28.30	28.26
<b>Volume Flow (acfm) = [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F) + 460°F)] / [Molecular weight x 2116.8] / 60 min/hr</b>				
Mass flow (lb/hr)	2,586,000	2,570,000	2,515,000	2,452,000
Temperature (°F)	1,096	1,068	1,069	1,072
Molecular weight	28.49	28.46	28.30	28.26
Volume flow (acfm)- calculated	1,718,154	1,678,706	1,652,949	1,617,205
- provided	1,722,900	1,683,400	1,657,000	1,621,300
	1.003	1.003	1.002	1.003
<b>Fuel Usage</b>				
Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu (Fuel Heat Content, Btu/lb (LHV))				
Heat input (MMBtu/hr, LHV)	1,045	982	946	898
Heat content (Btu/lb, LHV)	21,511	21,511	21,511	21,511
Fuel usage (lb/hr)- calculated	48,580	45,651	43,977	41,746
- provided	48,600	45,700	44,000	41,700
Heat content (Btu/cf, LHV)	920	920	920	920
Fuel density (lb/ft <sup>3</sup> )	0.0428	0.0428	0.0428	0.0428
Fuel usage (cf/hr)- calculated	1,135,870	1,067,391	1,028,261	976,087
<b>Stack and Exit Gas Conditions</b>				
Stack height (ft)	60	60	60	60
Diameter (ft)	21.0	21.0	21.0	21.0
<b>Velocity (ft/sec) = Volume flow (acfm) / [((diameter)<sup>2</sup> / 4) x 3.14159] / 60 sec/min</b>				
Volume flow (acfm)- from CT	1,722,900	1,683,400	1,657,000	1,621,300
Temperature (°F) (-20 oF from CT exhaust)	1,076	1,048	1,049	1,052
Exit gas volume flow (acfm)	1,700,755	1,661,366	1,635,326	1,600,134
Diameter (ft)	21.0	21.0	21.0	21.0
Velocity (ft/sec)- calculated	82.9	81.0	79.7	78.0
Velocity (ft/sec)- provided	82.9	81.0	79.7	78.0
Velocity (m/sec)- calculated (from provided value)	25.27	24.69	24.30	23.78

Source: General Electric, 1999; Decker Energy International, 2000.

Note: Universal gas constant = 1,545 ft-lb(force)/°R; atmospheric pressure = 2,116.8 lb(force)/ft<sup>2</sup>

Table A-10. Maximum Emissions for Criteria and Other Regulated Pollutants  
General Electric Frame 7FA, Simple Cycle, Dry Low NOx Combustor, Natural Gas, 50 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	3,390	3,390	3,390	3,390
Particulate (lb/hr) = Emission rate (lb/hr) from manufacturer (dry filterables)				
Basis, lb/hr (a)	11.0	11.0	11.0	11.0
(TPY)	18.6	18.6	18.6	18.6
Sulfur Dioxide (lb/hr) = Natural gas (cf/hr) x sulfur content (gr/100 cf) x 1 lb/7000 gr x (lb SO <sub>2</sub> /lb S)/100				
Fuel use (cf/hr)	1,135,870	1,067,391	1,028,261	976,087
Sulfur content (0.5 grains/ 100 cf) - assumed (b)	2	2	2	2
lb SO <sub>2</sub> /lb S (64/32)	2	2	2	2
Emission rate (lb/hr) - calculated	6.5	6.1	5.9	5.6
(lb/hr) - provided (0.5 gr/100 cf)	1.8	1.6	1.6	1.5
(TPY)	11.0	10.3	10.0	9.5
[Ratio lb/hr provided/calculated]	0.277	0.262	0.272	0.269
Nitrogen Oxides (lb/hr) = NOx(ppm) x [(20.9 x (1 - Moisture%/100)) - Oxygen(%)] x 2116.8 x Volume flow (scfm) x 46 (mole. wgt NOx) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]				
Basis, ppmvd @ 15% O <sub>2</sub> (a)	10.0	10.0	10.0	10.0
Moisture (%)	7.14	7.28	8.64	8.97
Oxygen (%)	13.49	13.79	13.61	13.70
Volume Flow (scfm)	1,722,900	1,683,400	1,657,000	1,621,300
Temperature (°F)	1,096	1,068	1,069	1,072
Emission rate (lb/hr) - calculated	42.0	39.4	38.0	36.1
(lb/hr) - provided	44.7	42.1	40.6	38.5
(TPY)	75.8	71.3	68.9	65.3
[Ratio lb/hr provided/calculated]	1.066	1.067	1.068	1.067
Carbon Monoxide (lb/hr) = CO(ppm) x [(20.9 x (1 - Moisture%/100)) - Oxygen(%)] x 2116.8 lb/ft <sup>2</sup> x Volume flow (scfm) x 28 (mole. wgt CO) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]				
Basis, ppmvd - calculated	10.0	10.0	9.9	10.0
Basis, ppmvd @ 15% O <sub>2</sub> - calculated	9.2	9.8	9.8	10.1
- provided (a)	9.2	9.8	9.8	10.1
Moisture (%)	7.14	7.28	8.64	8.97
Oxygen (%)	13.49	13.79	13.61	13.70
Volume Flow (scfm)	1,722,900	1,683,400	1,657,000	1,621,300
Temperature (°F)	1,096	1,068	1,069	1,072
Emission rate (lb/hr) - calculated from given ppmvd	23.6	23.5	23.6	22.2
(lb/hr) - provided	25.2	25.1	24.3	23.6
(TPY)	42.7	42.5	41.2	40.1
[Ratio lb/hr provided/calculated]	1.070	1.069	1.073	1.064
VOCs (lb/hr) = VOC(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft <sup>2</sup> x Volume flow (scfm) x 16 (mole. wgt as methane) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]				
Basis, ppmvd (as CH <sub>4</sub> ) - calculated	2.0	2.1	2.1	2.1
Basis, ppmvd @ 15% O <sub>2</sub> - calculated	1.9	2.0	2.0	2.2
- provided (a)	1.9	2.0	2.0	2.16
Moisture (%)	7.14	7.28	8.64	8.97
Oxygen (%)	13.49	13.79	13.61	13.70
Volume Flow (scfm)	1,722,900	1,683,400	1,657,000	1,621,300
Temperature (°F)	1,096	1,068	1,069	1,072
Emission rate (lb/hr) - calculated	2.8	2.8	2.7	2.7
(lb/hr) - provided	3.0	3.0	2.8	2.8
(TPY)	5.0	5.0	4.8	4.8
[Ratio lb/hr provided/calculated]	1.076	1.069	1.057	1.045
Lead (lb/hr) = NA				
Emission Rate Basis	NA	NA	NA	NA
Emission rate (lb/hr)	NA	NA	NA	NA
(TPY)	NA	NA	NA	NA
Mercury (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis, lb/10 <sup>12</sup> Btu (c)	8.00E-04	8.00E-04	8.00E-04	8.00E-04
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	9.28E-07	8.72E-07	8.40E-07	7.97E-07
(TPY)	1.57E-06	1.48E-06	1.42E-06	1.35E-06
Sulfuric Acid Mist = SO <sub>2</sub> emission rate (lb/hr) x conversion rate of SO <sub>2</sub> to H <sub>2</sub> SO <sub>4</sub> (%) x MW H <sub>2</sub> SO <sub>4</sub> / MW SO <sub>2</sub> (98/64)				
SO <sub>2</sub> emission rate (lb/hr)	6.5	6.1	5.9	5.6
lb H <sub>2</sub> SO <sub>4</sub> / lb SO <sub>2</sub> (98/64)	1.53	1.53	1.53	1.53
Conversion to H <sub>2</sub> SO <sub>4</sub> (%) (b)	15	15	15	15
Emission Rate (lb/hr)	1.49	1.40	1.35	1.28
(TPY)	2.53	2.37	2.29	2.17

Source: (a) General Electric 1999; (b) Decker Energy International, 2000; (c) EPRI, 1994  
Note: ppmvd = parts per million, volume dry; O<sub>2</sub> = oxygen.

Table A-11. Maximum Emissions for Other Regulated PSD Pollutants  
General Electric Frame 7FA, Simple Cycle, Dry Low NOx Combustor, Natural Gas, 50 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	3,390	3,390	3,390	3,390
2,3,7,8 TCDD Equivalents (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a) , lb/10 <sup>12</sup> Btu	1.20E-06	1.20E-06	1.20E-06	1.20E-06
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	1.39E-09	1.31E-09	1.26E-09	1.20E-09
(TPY)	2.36E-09	2.22E-09	2.14E-09	2.03E-09
Beryllium (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a) , lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Fluoride (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis, lb/10 <sup>12</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00

Source: Electric Power Research Institute (EPRI), Electric Utility Trace Substances Report, 1994 (Table B-12) .  
Emission factors for metals are questionable and not used .

Note: No emission factors for hydrogen chloride (HCl) from natural gas-firing.

Table A-12. Maximum Emissions for Hazardous Air Pollutants  
General Electric Frame 7FA, Simple Cycle, Dry Low NOx Combustor, Natural Gas, 50 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	3,390	3,390	3,390	3,390
Antimony (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Benzene (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0.8	0.8	0.8	0.8
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	9.28E-04	8.72E-04	8.40E-04	7.97E-04
(TPY)	1.57E-03	1.48E-03	1.42E-03	1.35E-03
Cadmium (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Chromium (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Formaldehyde (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	34	34	34	34
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	3.94E-02	3.71E-02	3.57E-02	3.39E-02
(TPY)	6.68E-02	6.28E-02	6.05E-02	5.74E-02
Cobalt (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Manganese (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Nickel (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Phosphorous (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (b), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Selenium (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	0	0	0	0
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
(TPY)	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Toluene (lb/hr) = Basis (lb/10 <sup>22</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>22</sup> Btu				
Basis (a), lb/10 <sup>22</sup> Btu	10	10	10	10
Heat Input Rate (MMBtu/hr)	1,160	1,090	1,050	997
Emission Rate (lb/hr)	1.16E-02	1.09E-02	1.05E-02	9.97E-03
(TPY)	1.97E-02	1.85E-02	1.78E-02	1.69E-02

Source: Electric Power Research Institute (EPRI), Electric Utility Trace Substances Report, 1994 (Table B-12).  
Emission factors for metals are questionable and not used.



Table A-13. Design Information and Stack Parameters  
General Electric Frame 7 FA, Simple Cycle Unit, Water Injection, Oil firing, 100 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
<b>Combustion Turbine Performance</b>				
Evaporative cooler status/ efficiency (%)	Off	On	On	On
Ambient Relative Humidity (%)	80	60	87	55
Gross power output (MW)	191.82	183.16	172.24	165.43
Gross heat rate (Btu/kWh, LHV)	9,665	9,773	9,963	10,083
(Btu/kWh, HHV)	10,245	10,359	10,560	10,688
Heat Input (MMBtu/hr, LHV) - calculated	1,854	1,790	1,716	1,668
- provided	1,854	1,790	1,716	1,668
(MMBtu/hr, HHV) - calculated	1,965	1,897	1,819	1,768
(HHV/LHV)	1.06	1.06	1.06	1.06
Fuel heating value (Btu/lb, LHV)	18,560	18,560	18,560	18,560
(Btu/lb, HHV)	19,674	19,674	19,674	19,674
(HHV/LHV)	1.06	1.06	1.06	1.06
<b>CT Exhaust Flow</b>				
Mass Flow (lb/hr)	3,837,000	3,688,000	3,523,000	3,429,000
Temperature (°F)	1,074	1,098	1,121	1,131
Moisture (% Vol.)	10.42	11.14	12.44	13.18
Oxygen (% Vol.)	11.27	11.10	10.84	10.72
Molecular Weight - calculated	28.40	28.32	28.18	28.09
- provided	28.39	28.31	28.17	28.09
<b>Volume Flow (acfm) = <math>\frac{1}{60} \times \frac{\text{Mass Flow (lb/hr)} \times (\text{Temp. (°F)} + 460)}{\text{Molecular weight} \times 2116.8}</math></b>				
Mass flow (lb/hr)	3,837,000	3,688,000	3,523,000	3,429,000
Temperature (°F)	1,074	1,098	1,121	1,131
Molecular weight	28.40	28.32	28.18	28.09
Volume flow (acfm) - calculated	2,521,379	2,468,089	2,404,748	2,362,513
- provided	2,528,300	2,475,000	2,411,400	2,368,900
	1.003	1.003	1.003	1.003
<b>Fuel Usage</b>				
<b>Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu (Fuel Heat Content, Btu/lb (LHV))</b>				
Heat input (MMBtu/hr, LHV)	1,854	1,790	1,716	1,668
Heat content (Btu/lb, LHV)	18,560	18,560	18,560	18,560
Fuel usage (lb/hr) - calculated	99,892	96,444	92,457	89,871
- provided	99,900	96,400	92,500	89,900
Fuel density (lb/gal)	7.1	7.1	7.1	7.1
Fuel usage (gal/hr) - from provided	14,070	13,577	13,028	12,662
(gal/yr)	10,130,000	9,780,000	9,380,000	9,120,000
<b>Stack and Exit Gas Conditions</b>				
Stack height (ft)	60	60	60	60
Diameter (ft)	21.0	21.0	21.0	21.0
<b>Velocity (ft/sec) = <math>\frac{\text{Volume flow (acfm)}}{[(\text{diameter})^2 / 4] \times 3.14159} \times 60 \text{ sec/min}</math></b>				
Volume flow (acfm) - from CT	2,528,300	2,475,000	2,411,400	2,368,900
Temperature (°F) (-20 of from CT exhaust)	1,054	1,078	1,101	1,111
Exit gas volume flow (acfm)	2,495,337	2,443,228	2,380,895	2,339,121
Diameter (ft)	21.0	21.0	21.0	21.0
Velocity (ft/sec) - calculated	121.7	119.1	116.0	114.0
Velocity (ft/sec) - provided	121.7	119.1	116.0	114.0
Velocity (m/sec) - calculated (from provided value)	37.1	36.3	35.4	34.7

Source: General Electric, 1999; Decker Energy International, 2000.

Note: Universal gas constant = 1,545 ft-lb(force)/°R; atmospheric pressure = 2,116.8 lb(force)/ft²

Table A-14. Maximum Emissions for Criteria and Other Regulated Pollutants  
General Electric Frame 7 FA, Simple Cycle Unit, Water Injection, Oil firing, 100 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	720	720	720	720
Particulate from CT = Emission rate (lb/hr) from CT manufacturer (dry filterables)				
Basis, lb/hr - provided (a) (b)	22.0	22.0	22.0	22.0
(TPY)	7.9	7.9	7.9	7.9
Sulfur Dioxide (lb/hr) = Fuel Oil (lb/hr) x sulfur content (gr/100 cf) x (lb SO <sub>2</sub> /lb S)/100				
Fuel use (lb/hr)	99,900	96,400	92,500	89,900
Fuel Sulfur content	0.05%	0.05%	0.05%	0.05%
lb SO <sub>2</sub> /lb S (64/32)	2	2	2	2
Emission rate (lb/hr)- calculated	99.9	96.4	92.5	89.9
(lb/hr)- provided	106.9	103.2	98.9	96.2
(TPY)	38.5	37.2	35.6	34.6
[Ratio lb/hr provided/calculated]	1.070	1.071	1.069	1.070
Nitrogen Oxides (lb/hr) = NOx(ppm) x [(20.9 x (1 - Moisture(%) / 100)) - Oxygen(%)] x 2116.8 x Volume flow (acfm) x 46 (mole. wtg NOx) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]				
Basis, ppmvd @15% O <sub>2</sub> (a)	42	42	42	42
Moisture (%)	10.42	11.14	12.44	13.18
Oxygen (%)	11.27	11.10	10.84	10.72
Volume Flow (acfm)	2,528,300	2,475,000	2,411,400	2,368,900
Temperature (°F)	1,074	1,098	1,121	1,131
Emission rate (lb/hr)- calculated	330.6	319.5	306.3	297.6
(lb/hr)- provided	352.1	340.1	326.0	316.9
(TPY)	126.8	122.4	117.4	114.1
[Ratio lb/hr provided/calculated]	1.065	1.064	1.064	1.065
Carbon Monoxide (lb/hr) = CO(ppm) x [(20.9 x (1 - Moisture(%) / 100)) - Oxygen(%)] x 2116.8 lb/hr x Volume flow (acfm) x 28 (mole. wtg CO) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]				
Basis, ppmvd- calculated	20.0	20.1	20.1	20.0
Basis, ppmvd @ 15% O <sub>2</sub> - calculated	14.2	14.1	13.9	13.8
- provided (a)	14.2	14.1	13.9	13.8
Moisture (%)	10.42	11.14	12.44	13.18
Oxygen (%)	11.27	11.10	10.84	10.72
Volume Flow (acfm)	2,528,300	2,475,000	2,411,400	2,368,900
Temperature (°F)	1,074	1,098	1,121	1,131
Emission rate (lb/hr)- calculated from given ppmvd	68.0	65.3	61.7	59.5
(lb/hr)- provided	72.6	69.4	65.6	63.5
(TPY)	26.1	25.0	23.6	22.9
[Ratio lb/hr provided/calculated]	1.067	1.063	1.063	1.067
VOCs (lb/hr) = VOC(ppm) x [1 - Moisture(%) / 100] x 2116.8 lb/hr x Volume flow (acfm) x 16 (mole. wtg as methane) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]				
Basis, ppmvd (as CH <sub>4</sub> )- calculated	3.9	4.0	4.0	4.1
Basis, ppmvd @ 15% O <sub>2</sub> - calculated	2.8	2.8	2.8	2.8
- provided (a)	2.8	2.8	2.8	2.8
Moisture (%)	10.42	11.14	12.44	13.18
Oxygen (%)	11.27	11.10	10.84	10.72
Volume Flow (acfm)	2,528,300	2,475,000	2,411,400	2,368,900
Temperature (°F)	1,074	1,098	1,121	1,131
Emission rate (lb/hr)- calculated	7.7	7.4	7.1	6.9
(lb/hr)- provided	8.1	7.8	7.5	7.3
(TPY)	2.9	2.8	2.7	2.6
[Ratio lb/hr provided/calculated]	1.056	1.053	1.056	1.058
Lead (lb/hr) = Basis (lb/10 <sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>13</sup> Btu				
Basis, lb/10 <sup>13</sup> Btu (c)	10.8	10.8	10.8	10.8
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	2.12E-02	2.05E-02	1.96E-02	1.91E-02
(TPY)	7.64E-03	7.38E-03	7.07E-03	6.87E-03
Mercury (lb/hr) = Basis (lb/10 <sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>13</sup> Btu				
Basis, lb/10 <sup>13</sup> Btu (c)	6.26E-01	6.26E-01	6.26E-01	6.26E-01
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	1.23E-03	1.19E-03	1.14E-03	1.11E-03
(TPY)	4.43E-04	4.28E-04	4.10E-04	3.98E-04
Sulfuric Acid Mist = SO <sub>2</sub> emission rate (lb/hr) x conversion rate of SO <sub>2</sub> to H <sub>2</sub> SO <sub>4</sub> (%) x MW H <sub>2</sub> SO <sub>4</sub> / MW SO <sub>2</sub> (98/64)				
SO <sub>2</sub> emission rate (lb/hr)	106.9	103.2	98.9	96.2
lb H <sub>2</sub> SO <sub>4</sub> / lb SO <sub>2</sub> (98/64)	1.53	1.53	1.53	1.53
Conversion to H <sub>2</sub> SO <sub>4</sub> (%) (b)	15	15	15	15
Emission Rate (lb/hr)	24.55	23.70	22.72	22.10
(TPY)	8.84	8.53	8.18	7.95

Source: (a) General Electric 1999; (b) Decker Energy International, 2000; (c) EPA, 1998 (AP-42, Draft, Table 3.1-6)  
Note: ppmvd = parts per million, volume dry; O<sub>2</sub> = oxygen.

Table A-15. Maximum Emissions for Other Regulated PSD Pollutants  
General Electric Frame 7 FA, Simple Cycle Unit, Water Injection, Oil firing, 100 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	720	720	720	720
2,3,7,8 TCDD Equivalents (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	3.80E-04	3.80E-04	3.80E-04	3.80E-04
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	7.47E-07	7.21E-07	6.91E-07	6.72E-07
(TPY)	2.69E-07	2.60E-07	2.49E-07	2.42E-07
Beryllium (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	0.331	0.331	0.331	0.331
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	6.50E-04	6.28E-04	6.02E-04	5.85E-04
(TPY)	2.34E-04	2.26E-04	2.17E-04	2.11E-04
Fluoride (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (b), lb/10 <sup>12</sup> Btu	32.54	32.54	32.54	32.54
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	6.39E-02	6.17E-02	5.92E-02	5.75E-02
(TPY)	2.30E-02	2.22E-02	2.13E-02	2.07E-02
Hydrogen Chloride (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (c), lb/10 <sup>12</sup> Btu	211	211	211	211
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	4.15E-01	4.00E-01	3.84E-01	3.73E-01
(TPY)	1.49E-01	1.44E-01	1.38E-01	1.34E-01

Sources: (a) EPA 1998 (AP-42, Draft, Table 3.1-6)  
 (b) Golder Associates, 1998  
 (c) Chlorine content of 4 ppm assumed based on ASTM D 2880.

Table A-16. Maximum Emissions for Hazardous Air Pollutants  
General Electric Frame 7 FA, Simple Cycle Unit, Water Injection, Oil firing, 100 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	720	720	720	720
<b>Arsenic (lb/hr) = Basis (lb/10<sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>13</sup> Btu</b>				
Basis (a), lb/10 <sup>13</sup> Btu	7.91	7.91	7.91	7.91
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	1.55E-02	1.50E-02	1.44E-02	1.40E-02
(TPY)	5.60E-03	5.40E-03	5.18E-03	5.03E-03
<b>Benzene (lb/hr) = Basis (lb/10<sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>13</sup> Btu</b>				
Basis (b), lb/10 <sup>13</sup> Btu	1.1	1.1	1.1	1.1
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	2.16E-03	2.09E-03	2.00E-03	1.94E-03
(TPY)	7.78E-04	7.51E-04	7.20E-04	7.00E-04
<b>Cadmium (lb/hr) = Basis (lb/10<sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>13</sup> Btu</b>				
Basis (a), lb/10 <sup>13</sup> Btu	3.24	3.24	3.24	3.24
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	6.37E-03	6.15E-03	5.89E-03	5.73E-03
(TPY)	2.29E-03	2.21E-03	2.12E-03	2.06E-03
<b>Chromium (lb/hr) = Basis (lb/10<sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>13</sup> Btu</b>				
Basis (a), lb/10 <sup>13</sup> Btu	6.76	6.76	6.76	6.76
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	1.33E-02	1.28E-02	1.23E-02	1.20E-02
(TPY)	4.78E-03	4.62E-03	4.43E-03	4.30E-03
<b>Formaldehyde (lb/hr) = Basis (lb/10<sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>13</sup> Btu</b>				
Basis (b), lb/10 <sup>13</sup> Btu	20	20	20	20
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	3.93E-02	3.79E-02	3.64E-02	3.54E-02
(TPY)	1.41E-02	1.37E-02	1.31E-02	1.27E-02
<b>Cobalt (lb/hr) = Basis (lb/10<sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>13</sup> Btu</b>				
Basis (c), lb/10 <sup>13</sup> Btu	37	37	37	37
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	7.27E-02	7.02E-02	6.73E-02	6.54E-02
(TPY)	2.62E-02	2.53E-02	2.42E-02	2.36E-02
<b>Manganese (lb/hr) = Basis (lb/10<sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>13</sup> Btu</b>				
Basis (a), lb/10 <sup>13</sup> Btu	432	432	432	432
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	8.49E-01	8.20E-01	7.86E-01	7.64E-01
(TPY)	3.06E-01	2.95E-01	2.83E-01	2.75E-01
<b>Nickel (lb/hr) = Basis (lb/10<sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>13</sup> Btu</b>				
Basis (a), lb/10 <sup>13</sup> Btu	86.3	86.3	86.3	86.3
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	1.70E-01	1.64E-01	1.57E-01	1.53E-01
(TPY)	6.11E-02	5.89E-02	5.65E-02	5.49E-02
<b>Phosphorous (lb/hr) = Basis (lb/10<sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>13</sup> Btu</b>				
Basis (c), lb/10 <sup>13</sup> Btu	300	300	300	300
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	5.90E-01	5.69E-01	5.46E-01	5.30E-01
(TPY)	2.12E-01	2.05E-01	1.96E-01	1.91E-01
<b>Selenium (lb/hr) = Basis (lb/10<sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>13</sup> Btu</b>				
Basis (a), lb/10 <sup>13</sup> Btu	23	23	23	23
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	4.52E-02	4.36E-02	4.18E-02	4.07E-02
(TPY)	1.63E-02	1.57E-02	1.51E-02	1.46E-02
<b>Toluene (lb/hr) = Basis (lb/10<sup>13</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>13</sup> Btu</b>				
Basis (a), lb/10 <sup>13</sup> Btu	237	237	237	237
Heat Input Rate (MMBtu/hr)	1,965	1,897	1,819	1,768
Emission Rate (lb/hr)	4.66E-01	4.50E-01	4.31E-01	4.19E-01
(TPY)	1.68E-01	1.62E-01	1.55E-01	1.51E-01

Sources: (a) EPA 1998 (AP-42, Draft, Table 3.1-5 and 3.1-6)  
(b) Electric Power Research Institute (EPRI), Electric Utility Trace Substances Report, 1994 (Table B-12)  
(c) EPA, 1996 (AP-42, Table 3.1-4)

Table A-17. Design Information and Stack Parameters  
General Electric Frame 7FA, Simple Cycle Unit, Water Injection, Oil firing, 75 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
<b>Combustion Turbine Performance</b>				
Evaporative cooler status/ efficiency (%)	Off	Off	Off	Off
Ambient Relative Humidity (%)	80	60	87	55
Gross power output (MW)	142.15	133.53	126.09	115.89
Gross heat rate (Btu/kWh, LHV)	10,636	10,784	10,992	11,278
(Btu/kWh, HHV)	11,275	11,431	11,652	11,955
Heat Input (MMBtu/hr, LHV)- calculated	1,512	1,440	1,386	1,307
- provided	1,512	1,440	1,386	1,307
(MMBtu/hr, HHV) - calculated	1,603	1,526	1,469	1,385
(HHV/LHV)	1.06	1.06	1.06	1.06
Fuel heating value (Btu/lb, LHV)	18,560	18,560	18,560	18,560
(Btu/lb, HHV)	19,674	19,674	19,674	19,674
(HHV/LHV)	1.06	1.06	1.06	1.06
<b>CT Exhaust Flow</b>				
Mass Flow (lb/hr)	3,018,000	2,886,000	2,776,000	2,689,000
Temperature (°F)	1,165	1,192	1,200	1,200
Moisture (% Vol.)	10.77	11.28	12.60	12.78
Oxygen (% Vol.)	10.92	10.81	10.63	10.80
Molecular Weight - calculated	28.38	28.32	28.17	28.14
- provided	28.37	28.32	28.17	28.13
Volume Flow (acfm) = [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F) + 460°F)] / [Molecular weight x 2116.8] / 60 min/hr				
Mass flow (lb/hr)	3,018,000	2,886,000	2,776,000	2,689,000
Temperature (°F)	1,165	1,192	1,200	1,200
Molecular weight	28.38	28.32	28.17	28.14
Volume flow (acfm)- calculated	2,102,228	2,047,643	1,989,896	1,929,903
- provided	2,108,000	2,038,700	1,995,300	1,935,100
	1.003	0.996	1.003	1.003
<b>Fuel Usage</b>				
Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu (Fuel Heat Content, Btu/lb (LHV))				
Heat input (MMBtu/hr, LHV)	1,512	1,440	1,386	1,307
Heat content (Btu/lb, LHV)	18,560	18,560	18,560	18,560
Fuel usage (lb/hr)- calculated	81,466	77,586	74,677	70,420
- provided	81,500	77,600	74,700	70,400
<b>Stack and Exit Gas Conditions</b>				
Stack height (ft)	60	60	60	60
Diameter (ft)	21.0	21.0	21.0	21.0
Velocity (ft/sec) = Volume flow (acfm) / [((diameter) <sup>2</sup> / 4) x 3.14159] / 60 sec/min				
Volume flow (acfm)- from CT	2,108,000	2,038,700	1,995,300	1,935,100
Temperature (°F) (-20 oF from CT exhaust)	1,145	1,172	1,180	1,180
Exit gas volume flow (acfm)	2,082,055	2,014,018	1,971,260	1,911,786
Diameter (ft)	21.0	21.0	21.0	21.0
Velocity (ft/sec)- calculated	101.4	98.1	96.0	93.1
Velocity (ft/sec)- provided	101.4	98.1	96.0	93.1
Velocity (m/sec)- calculated (from provided value)	30.9	29.9	29.3	28.4

Source: General Electric, 1999; Decker Energy International, 2000.

Note: Universal gas constant = 1,545 ft-lb(force)/°R; atmospheric pressure = 2,116.8 lb(force)/ft<sup>2</sup>

Table A-18. Maximum Emissions for Criteria and Other Regulated Pollutants  
General Electric Frame 7FA, Simple Cycle Unit, Water Injection, Oil firing, 75 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	720	720	720	720
Particulate from CT = Emission rate (lb/hr) from CT manufacturer (dry filterables)				
Basis, lb/hr - provided (a) (b)	22.0	22.0	22.0	22.0
(TPY)	7.9	7.9	7.9	7.9
Sulfur Dioxide (lb/hr) = Fuel Oil (lb/hr) x sulfur content (gr/100 cf) x (lb SO <sub>2</sub> /lb S)/100				
Fuel use (lb/hr)	81,500	77,600	74,700	70,400
Fuel Sulfur content	0.05%	0.05%	0.05%	0.05%
lb SO <sub>2</sub> /lb S (64/32)	2	2	2	2
Emission rate (lb/hr)- calculated	81.5	77.6	74.7	70.4
(lb/hr)- provided	87.2	83.0	79.9	75.3
(TPY)	31.4	29.9	28.8	27.1
[Ratio lb/hr provided/calculated]	1.070	1.070	1.070	1.070
Nitrogen Oxides (lb/hr) = NOx(ppm) x [(20.9 x (1 - Moisture%/100)) - Oxygen(%)] x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]				
Basis, ppmvd @ 15% O <sub>2</sub> (a)	42	42	42	42
Moisture (%)	10.77	11.28	12.60	12.78
Oxygen (%)	10.92	10.81	10.63	10.80
Volume Flow (acfm)	2,108,000	2,038,700	1,995,300	1,935,100
Temperature (°F)	1,165	1,192	1,200	1,200
Emission rate (lb/hr)- calculated	269.9	256.9	247.1	233.1
(lb/hr)- provided	287.3	273.5	263.1	248.2
(TPY)	103.4	98.5	94.7	89.4
[Ratio lb/hr provided/calculated]	1.064	1.065	1.065	1.065
Carbon Monoxide (lb/hr) = CO(ppm) x [(20.9 x (1 - Moisture%/100)) - Oxygen(%)] x 2116.8 lb/ft <sup>2</sup> x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]				
Basis, ppmvd- calculated	20.1	20.1	20.0	20.1
Basis, ppmvd @ 15% O <sub>2</sub> - calculated	13.7	13.6	13.5	13.9
- provided (a)	13.7	13.6	13.5	13.9
Moisture (%)	10.77	11.28	12.60	12.78
Oxygen (%)	10.92	10.81	10.63	10.80
Volume Flow (acfm)	2,108,000	2,038,700	1,995,300	1,935,100
Temperature (°F)	1,165	1,192	1,200	1,200
Emission rate (lb/hr)- calculated from given ppmvd	53.6	50.6	48.3	47.0
(lb/hr)- provided	56.9	53.8	51.6	50.0
(TPY)	20.5	19.4	18.6	18.0
[Ratio lb/hr provided/calculated]	1.062	1.063	1.067	1.065
VOCs (lb/hr) = VOC(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft <sup>2</sup> x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]				
Basis, ppmvd (as CH <sub>4</sub> )- calculated	4.0	4.0	4.0	4.0
Basis, ppmvd @ 15% O <sub>2</sub> - calculated	2.7	2.7	2.7	2.8
- provided (a)	2.7	2.7	2.7	2.8
Moisture (%)	10.77	11.28	12.60	12.78
Oxygen (%)	10.92	10.81	10.63	10.80
Volume Flow (acfm)	2,108,000	2,038,700	1,995,300	1,935,100
Temperature (°F)	1,165	1,192	1,200	1,200
Emission rate (lb/hr)- calculated	6.0	5.7	5.5	5.4
(lb/hr)- provided	6.4	6.1	5.9	5.7
(TPY)	2.3	2.2	2.1	2.1
[Ratio lb/hr provided/calculated]	1.060	1.062	1.068	1.054
Lead (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis, lb/10 <sup>12</sup> Btu (c)	10.8	10.8	10.8	10.8
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	1.73E-02	1.65E-02	1.59E-02	1.50E-02
(TPY)	6.23E-03	5.93E-03	5.71E-03	5.39E-03
Mercury (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis, lb/10 <sup>12</sup> Btu (c)	6.26E-01	6.26E-01	6.26E-01	6.26E-01
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	1.00E-03	9.56E-04	9.20E-04	8.67E-04
(TPY)	3.61E-04	3.44E-04	3.31E-04	3.12E-04
Sulfuric Acid Mist = SO <sub>2</sub> emission rate (lb/hr) x conversion rate of SO <sub>2</sub> to H <sub>2</sub> SO <sub>4</sub> (%) x MW H <sub>2</sub> SO <sub>4</sub> / MW SO <sub>2</sub> (98/64)				
SO <sub>2</sub> emission rate (lb/hr)	87.2	83.0	79.9	75.3
lb H <sub>2</sub> SO <sub>4</sub> /lb SO <sub>2</sub> (98/64)	1.53	1.53	1.53	1.53
Conversion to H <sub>2</sub> SO <sub>4</sub> (%) (b)	15	15	15	15
Emission Rate (lb/hr)	20.03	19.06	18.35	17.30
(TPY)	7.21	6.86	6.61	6.23

Source: (a) General Electric 1999; (b) Decker Energy International, 2000; (c) EPA, 1998 (AP-42, Draft, Table 3.1-6)  
Note: ppmvd = parts per million, volume dry; O<sub>2</sub> = oxygen.

Table A-19. Maximum Emissions for Other Regulated PSD Pollutants  
General Electric Frame 7FA, Simple Cycle Unit, Water Injection, Oil firing, 75 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	720	720	720	720
2,3,7,8 TCDD Equivalents (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a) , lb/10 <sup>12</sup> Btu	3.80E-04	3.80E-04	3.80E-04	3.80E-04
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	6.09E-07	5.80E-07	5.58E-07	5.26E-07
(TPY)	2.19E-07	2.09E-07	2.01E-07	1.90E-07
Beryllium (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a) , lb/10 <sup>12</sup> Btu	0.331	0.331	0.331	0.331
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	5.31E-04	5.05E-04	4.86E-04	4.59E-04
(TPY)	1.91E-04	1.82E-04	1.75E-04	1.65E-04
Fluoride (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (b) , lb/10 <sup>12</sup> Btu	32.54	32.54	32.54	32.54
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	5.22E-02	4.97E-02	4.78E-02	4.51E-02
(TPY)	1.88E-02	1.79E-02	1.72E-02	1.62E-02
Hydrogen Chloride (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (c) , lb/10 <sup>12</sup> Btu	211	211	211	211
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	3.38E-01	3.22E-01	3.10E-01	2.92E-01
(TPY)	1.22E-01	1.16E-01	1.12E-01	1.05E-01

Sources: (a) EPA 1998 (AP-42, Draft, Table 3.1-6)  
(b) Golder Associates, 1998  
(c) Chlorine content of 4 ppm assumed based on ASTM D 2880.

Table A-20. Maximum Emissions for Hazardous Air Pollutants  
General Electric Frame 7FA, Simple Cycle Unit, Water Injection, Oil firing, 75 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	720	720	720	720
<b>Arsenic (lb/hr) = Basis (lb/10<sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>12</sup> Btu</b>				
Basis (a), lb/10 <sup>12</sup> Btu	7.91	7.91	7.91	7.91
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	1.27E-02	1.21E-02	1.16E-02	1.10E-02
(TPY)	4.56E-03	4.35E-03	4.18E-03	3.95E-03
<b>Benzene (lb/hr) = Basis (lb/10<sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>12</sup> Btu</b>				
Basis (b), lb/10 <sup>12</sup> Btu	1.1	1.1	1.1	1.1
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	1.76E-03	1.68E-03	1.62E-03	1.52E-03
(TPY)	6.35E-04	6.04E-04	5.82E-04	5.49E-04
<b>Cadmium (lb/hr) = Basis (lb/10<sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>12</sup> Btu</b>				
Basis (a), lb/10 <sup>12</sup> Btu	3.24	3.24	3.24	3.24
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	5.19E-03	4.95E-03	4.76E-03	4.49E-03
(TPY)	1.87E-03	1.78E-03	1.71E-03	1.62E-03
<b>Chromium (lb/hr) = Basis (lb/10<sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>12</sup> Btu</b>				
Basis (a), lb/10 <sup>12</sup> Btu	6.76	6.76	6.76	6.76
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	1.08E-02	1.03E-02	9.93E-03	9.37E-03
(TPY)	3.90E-03	3.71E-03	3.58E-03	3.37E-03
<b>Formaldehyde (lb/hr) = Basis (lb/10<sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>12</sup> Btu</b>				
Basis (b), lb/10 <sup>12</sup> Btu	20	20	20	20
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	3.21E-02	3.05E-02	2.94E-02	2.77E-02
(TPY)	1.15E-02	1.10E-02	1.06E-02	9.98E-03
<b>Cobalt (lb/hr) = Basis (lb/10<sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>12</sup> Btu</b>				
Basis (c), lb/10 <sup>12</sup> Btu	37	37	37	37
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	5.93E-02	5.65E-02	5.44E-02	5.13E-02
(TPY)	2.13E-02	2.03E-02	1.96E-02	1.85E-02
<b>Manganese (lb/hr) = Basis (lb/10<sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>12</sup> Btu</b>				
Basis (a), lb/10 <sup>12</sup> Btu	432	432	432	432
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	6.92E-01	6.59E-01	6.35E-01	5.99E-01
(TPY)	2.49E-01	2.37E-01	2.28E-01	2.15E-01
<b>Nickel (lb/hr) = Basis (lb/10<sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>12</sup> Btu</b>				
Basis (a), lb/10 <sup>12</sup> Btu	86.3	86.3	86.3	86.3
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	1.38E-01	1.32E-01	1.27E-01	1.20E-01
(TPY)	4.98E-02	4.74E-02	4.56E-02	4.30E-02
<b>Phosphorous (lb/hr) = Basis (lb/10<sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>12</sup> Btu</b>				
Basis (c), lb/10 <sup>12</sup> Btu	300	300	300	300
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	4.81E-01	4.58E-01	4.41E-01	4.16E-01
(TPY)	1.73E-01	1.65E-01	1.59E-01	1.50E-01
<b>Selenium (lb/hr) = Basis (lb/10<sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>12</sup> Btu</b>				
Basis (a), lb/10 <sup>12</sup> Btu	23	23	23	23
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	3.69E-02	3.51E-02	3.38E-02	3.19E-02
(TPY)	1.33E-02	1.26E-02	1.22E-02	1.15E-02
<b>Toluene (lb/hr) = Basis (lb/10<sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10<sup>12</sup> Btu</b>				
Basis (a), lb/10 <sup>12</sup> Btu	237	237	237	237
Heat Input Rate (MMBtu/hr)	1,603	1,526	1,469	1,385
Emission Rate (lb/hr)	3.80E-01	3.62E-01	3.48E-01	3.28E-01
(TPY)	1.37E-01	1.30E-01	1.25E-01	1.18E-01

Sources: (a) EPA 1998 (AP-42, Draft, Table 3.1-5 and 3.1-6)  
(b) Electric Power Research Institute (EPRI), Electric Utility Trace Substances Report, 1994 (Table B-12)  
(c) EPA, 1996 (AP-42, Table 3.1-4)



Table A-21. Design Information and Stack Parameters  
General Electric Frame 7FA, Simple Cycle Unit, Water Injection, Oil firing, 50 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
<b>Combustion Turbine Performance</b>				
Evaporative cooler status/ efficiency (%)	Off	Off	Off	Off
Ambient Relative Humidity (%)	80	60	87	55
Gross power output (MW)	93.51	87.62	82.61	75.90
Gross heat rate (Btu/kWh, LHV)	12,042	12,132	12,408	12,833
(Btu/kWh, HHV)	12,764	12,860	13,152	13,603
Heat Input (MMBtu/hr, LHV) - calculated	1,126	1,063	1,025	974
- provided	1,126	1,063	1,025	974
(MMBtu/hr, HHV) - calculated	1,194	1,127	1,087	1,032
(HHV/LHV)	1.06	1.06	1.06	1.06
Fuel heating value (Btu/lb, LHV)	18,560	18,560	18,560	18,560
(Btu/lb, HHV)	19,674	19,674	19,674	19,674
(HHV/LHV)	1.06	1.06	1.06	1.06
<b>CT Exhaust Flow</b>				
Mass Flow (lb/hr)	2,668,000	2,647,000	2,589,000	2,523,000
Temperature (°F)	1,060	1,038	1,040	1,045
Moisture (% Vol.)	10.42	11.14	12.44	13.18
Oxygen (% Vol.)	11.27	11.10	10.84	10.72
Molecular Weight - calculated	28.40	28.32	28.18	28.09
- provided	28.39	28.31	28.17	28.09
<b>Volume Flow (acfm) = [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F) + 460°F)] / [Molecular weight x 2116.8] / 60 min/hr</b>				
Mass flow (lb/hr)	2,668,000	2,647,000	2,589,000	2,523,000
Temperature (°F)	1,060	1,038	1,040	1,045
Molecular weight	28.40	28.32	28.18	28.09
Volume flow (acfm) - calculated	1,737,202	1,703,210	1,676,673	1,644,335
- provided	1,737,800	1,701,300	1,675,100	1,640,200
	1.000	0.999	0.999	0.997
<b>Fuel Usage</b>				
<b>Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu (Fuel Heat Content, Btu/lb (LHV))</b>				
Heat input (MMBtu/hr, LHV)	1,126	1,063	1,025	974
Heat content (Btu/lb, LHV)	18,560	18,560	18,560	18,560
Fuel usage (lb/hr) - calculated	60,668	57,274	55,226	52,478
- provided	60,700	57,300	55,200	52,500
<b>Stack and Exit Gas Condition</b>				
Stack height (ft)	60	60	60	60
Diameter (ft)	21.0	21.0	21.0	21.0
<b>Velocity (ft/sec) = Volume flow (acfm) / [((diameter)<sup>2</sup>/4) x 3.14159] / 60 sec/min</b>				
Volume flow (acfm) - from CT	1,737,800	1,701,300	1,675,100	1,640,200
Temperature (°F) (-20 °F from CT exhaust)	1,040	1,018	1,020	1,025
Exit gas volume flow (acfm)	1,714,934	1,678,586	1,652,765	1,618,403
Diameter (ft)	21.0	21.0	21.0	21.0
Velocity (ft/sec) - calculated	83.6	81.9	80.6	78.9
Velocity (ft/sec) - provided	83.6	81.9	80.6	78.9
Velocity (m/sec) - calculated (from provided value)	25.5	25.0	24.6	24.1

Source: General Electric, 1999.

Note: Universal gas constant = 1,545 ft-lb(force)/°R; atmospheric pressure = 2,116.8 lb(force)/ft<sup>2</sup>

Table A-22. Maximum Emissions for Criteria and Other Regulated Pollutants  
General Electric Frame 7FA, Simple Cycle Unit, Water Injection, Oil firing, 50 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	720	720	720	720
Particulate from CT = Emission rate (lb/hr) from CT manufacturer (dry filterables)				
Basis, lb/hr - provided (a)	22.0	22.0	22.0	22.0
(TPY)	7.9	7.9	7.9	7.9
Sulfur Dioxide (lb/hr) = Fuel Oil (lb/hr) x sulfur content(gz/100 cf) x (lb SO <sub>2</sub> /lb S)/100				
Fuel use (lb/hr)	60,700	57,300	55,200	52,500
Fuel Sulfur content	0.05%	0.05%	0.05%	0.05%
lb SO <sub>2</sub> /lb S (64/32)	2	2	2	2
Emission rate (lb/hr)- calculated	60.7	57.3	55.2	52.5
(lb/hr)- provided	64.9	61.3	59.1	56.2
(TPY)	23.4	22.1	21.3	20.2
[Ratio lb/hr provided/calculated]	1.069	1.070	1.071	1.070
Nitrogen Oxides (lb/hr) = NOx(ppm) x [(20.9 x (1 - Moisture(%)/100)) - Oxygen(%)] x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]				
Basis, ppmvd @15% O <sub>2</sub> (a)	42	42	42	42
Moisture (%)	10.42	11.14	12.44	13.18
Oxygen (%)	11.27	11.10	10.84	10.72
Volume Flow (acfm)	1,737,800	1,701,300	1,675,100	1,640,200
Temperature (°F)	1,060	1,038	1,040	1,045
Emission rate (lb/hr)- calculated	229.4	228.4	224.3	217.8
(lb/hr)- provided	213.9	201.8	194.8	185.2
(TPY)	77.0	72.6	70.1	66.7
[Ratio lb/hr provided/calculated]	0.933	0.883	0.869	0.850
Carbon Monoxide (lb/hr) = CO(ppm) x [(20.9 x (1 - Moisture(%)/100)) - Oxygen(%)] x 2116.8 lb/ft <sup>2</sup> x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]				
Basis, ppmvd- calculated	23.3	24.7	25.1	25.8
Basis, ppmvd @ 15% O <sub>2</sub> - calculated	16.5	17.3	17.4	17.8
- provided (a)	16.5	17.3	17.4	17.8
Moisture (%)	10.42	11.14	12.44	13.18
Oxygen (%)	11.27	11.10	10.84	10.72
Volume Flow (acfm)	1,737,800	1,701,300	1,675,100	1,640,200
Temperature (°F)	1,060	1,038	1,040	1,045
Emission rate (lb/hr)- calculated from given ppmvd	54.8	57.3	56.6	56.2
(lb/hr)- provided	51.0	50.7	49.1	47.8
(TPY)	18.4	18.3	17.7	17.2
[Ratio lb/hr provided/calculated]	0.930	0.885	0.868	0.851
VOCs (lb/hr) = VOC(ppm) x [1 - Moisture(%)/100] x 2116.8 lb/ft <sup>2</sup> x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]				
Basis, ppmvd (as CH <sub>4</sub> )- calculated	4.5	4.7	4.9	5.1
Basis, ppmvd @ 15% O <sub>2</sub> - calculated	3.2	3.3	3.4	3.5
- provided (a)	3.2	3.3	3.4	3.5
Moisture (%)	10.42	11.14	12.44	13.18
Oxygen (%)	11.27	11.10	10.84	10.72
Volume Flow (acfm)	1,737,800	1,701,300	1,675,100	1,640,200
Temperature (°F)	1,060	1,038	1,040	1,045
Emission rate (lb/hr)- calculated	6.1	6.2	6.3	6.3
(lb/hr)- provided	5.6	5.6	5.5	5.4
(TPY)	2.0	2.0	2.0	1.9
[Ratio lb/hr provided/calculated]	0.921	0.897	0.871	0.855
Lead (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis, lb/10 <sup>12</sup> Btu (c)	10.8	10.8	10.8	10.8
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	1.29E-02	1.22E-02	1.17E-02	1.12E-02
(TPY)	4.64E-03	4.38E-03	4.22E-03	4.01E-03
Mercury (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis, lb/10 <sup>12</sup> Btu (c)	6.26E-01	6.26E-01	6.26E-01	6.26E-01
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	7.47E-04	7.05E-04	6.80E-04	6.46E-04
(TPY)	2.69E-04	2.54E-04	2.45E-04	2.33E-04
Sulfuric Acid Mist = SO <sub>2</sub> emission rate (lb/hr) x conversion rate of SO <sub>2</sub> to H <sub>2</sub> SO <sub>4</sub> (%) x MW H <sub>2</sub> SO <sub>4</sub> /MW SO <sub>2</sub> (98/64)				
SO <sub>2</sub> emission rate (lb/hr)	64.9	61.3	59.1	56.2
lb H <sub>2</sub> SO <sub>4</sub> /lb SO <sub>2</sub> (98/64)	1.53	1.53	1.53	1.53
Conversion to H <sub>2</sub> SO <sub>4</sub> (%) (b)	5	5	5	5
Emission Rate (lb/hr)	4.97	4.69	4.52	4.30
(TPY)	1.79	1.69	1.63	1.55

Source: (a) General Electric 1999; (b) Decker Energy International, 2000; (c) EPA, 1998 (AP-42, Draft, Table 3.1-6)  
Note: ppmvd = parts per million, volume dry; O<sub>2</sub> = oxygen.

Table A-23. Maximum Emissions for Other Regulated PSD Pollutants  
General Electric Frame 7FA, Simple Cycle Unit, Water Injection, Oil firing, 50 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	720	720	720	720
2,3,7,8 TCDD Equivalents (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	3.80E-04	3.80E-04	3.80E-04	3.80E-04
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	4.54E-07	4.28E-07	4.13E-07	3.92E-07
(TPY)	1.63E-07	1.54E-07	1.49E-07	1.41E-07
Beryllium (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	0.331	0.331	0.331	0.331
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	3.95E-04	3.73E-04	3.60E-04	3.42E-04
(TPY)	1.42E-04	1.34E-04	1.29E-04	1.23E-04
Fluoride (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (b), lb/10 <sup>12</sup> Btu	32.54	32.54	32.54	32.54
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	3.88E-02	3.67E-02	3.54E-02	3.36E-02
(TPY)	1.40E-02	1.32E-02	1.27E-02	1.21E-02
Hydrogen Chloride (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (c), lb/10 <sup>12</sup> Btu	211	211	211	211
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	2.52E-01	2.38E-01	2.29E-01	2.18E-01
(TPY)	1.79E-08	1.60E-08	1.48E-08	1.34E-08

Sources: (a) EPA 1998 (AP-42, Draft, Table 3.1-6)  
 (b) Golder Associates, 1998  
 (c) Chlorine content of 4 ppm assumed based on ASTM D 2880.

Table A-24. Maximum Emissions for Hazardous Air Pollutants  
General Electric Frame 7FA, Simple Cycle Unit, Water Injection, Oil firing, 50 % Load

Parameter	Ambient/Compressor Inlet Temperature			
	32 °F	59 °F	75 °F	95 °F
Hours of Operation	720	720	720	720
Arsenic (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	7.91	7.91	7.91	7.91
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	9.44E-03	8.91E-03	8.59E-03	8.17E-03
(TPY)	3.40E-03	3.21E-03	3.09E-03	2.94E-03
Benzene (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (b), lb/10 <sup>12</sup> Btu	1.1	1.1	1.1	1.1
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	1.31E-03	1.24E-03	1.20E-03	1.14E-03
(TPY)	4.73E-04	4.46E-04	4.30E-04	4.09E-04
Cadmium (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	3.24	3.24	3.24	3.24
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	3.87E-03	3.65E-03	3.52E-03	3.35E-03
(TPY)	1.39E-03	1.31E-03	1.27E-03	1.20E-03
Chromium (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	6.76	6.76	6.76	6.76
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	8.07E-03	7.62E-03	7.34E-03	6.98E-03
(TPY)	2.90E-03	2.74E-03	2.64E-03	2.51E-03
Formaldehyde (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (b), lb/10 <sup>12</sup> Btu	20	20	20	20
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	2.39E-02	2.25E-02	2.17E-02	2.06E-02
(TPY)	8.59E-03	8.11E-03	7.82E-03	7.43E-03
Cobalt (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (c), lb/10 <sup>12</sup> Btu	37	37	37	37
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	4.42E-02	4.17E-02	4.02E-02	3.82E-02
(TPY)	1.59E-02	1.50E-02	1.45E-02	1.38E-02
Manganese (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	432	432	432	432
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	5.16E-01	4.87E-01	4.69E-01	4.46E-01
(TPY)	1.86E-01	1.75E-01	1.69E-01	1.61E-01
Nickel (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	86.3	86.3	86.3	86.3
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	1.03E-01	9.72E-02	9.38E-02	8.91E-02
(TPY)	3.71E-02	3.50E-02	3.38E-02	3.21E-02
Phosphorous (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (c), lb/10 <sup>12</sup> Btu	300	300	300	300
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	3.58E-01	3.38E-01	3.26E-01	3.10E-01
(TPY)	1.29E-01	1.22E-01	1.17E-01	1.12E-01
Selenium (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	23	23	23	23
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	2.75E-02	2.59E-02	2.50E-02	2.37E-02
(TPY)	9.88E-03	9.33E-03	9.00E-03	8.55E-03
Toluene (lb/hr) = Basis (lb/10 <sup>12</sup> Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 <sup>12</sup> Btu				
Basis (a), lb/10 <sup>12</sup> Btu	237	237	237	237
Heat Input Rate (MMBtu/hr)	1,194	1,127	1,087	1,032
Emission Rate (lb/hr)	2.83E-01	2.67E-01	2.58E-01	2.45E-01
(TPY)	1.02E-01	9.61E-02	9.27E-02	8.81E-02

Sources: (a) EPA 1998 (AP-42, Draft, Table 3.1-5 and 3.1-6)  
(b) Electric Power Research Institute (EPRI), Electric Utility Trace Substances Report, 1994 (Table B-12)  
(c) EPA, 1996 (AP-42, Table 3.1-4)

**APPENDIX B**

**BEST AVAILABLE CONTROL TECHNOLOGY FOR  
THE PROPOSED COMBUSTION TURBINES**

## B.1 NEW SOURCE PERFORMANCE STANDARDS

BACT is a case-by-case emission limitation for each applicable pollutant, based on the maximum degree of emission reduction after taking into account the energy, environmental, and economic impacts, and other costs. The BACT cannot be any less stringent than any applicable new source performance standards (NSPS) and consideration must be given to the applicable NSPS in the determination of BACT [Rule 62-212.400(6) F.A.C.]. This requirement also applies for any applicable National Emission Standard for Hazardous Air Pollutants promulgated under 40 CFR Part 61. For combustion turbines the applicable NSPS is 40 CFR Part 60, Subpart GG Standards of Performance for Stationary Gas Turbines.

### B.1.1 SUBPART GG

The NSPS regulations (40 CFR, Subpart GG) applicable to gas turbines apply to:

1. Electric utility stationary gas turbines with a heat input at peak load of greater than  $100 \times 10^6$  Btu/hr [40 CFR 60.332 (b)];
2. Stationary gas turbines with a heat input at peak load between 10 and  $100 \times 10^6$  Btu/hr [40 CFR 60.332 (c)]; or
3. Stationary gas turbines with a manufacturer's rate base load at ISO conditions of 30 MW or less [40 CFR 60.332 (d)].

The electric utility stationary gas turbine provisions apply to stationary gas turbines constructed for the purpose of supplying more than one-third of their potential electric output capacity for sale to any utility power distribution system [40 CFR 60.331 (q)]. The requirements for electric utility stationary gas turbines are applicable to the turbines proposed for the Project and are the most stringent provision of the NSPS. These requirements are summarized in Table B-1 and were considered in the BACT analysis.

As noted from Table B-1, the NSPS  $\text{NO}_x$  emission limit can be adjusted upward to allow for fuel-bound nitrogen (FBN). For a fuel-bound nitrogen concentration of 0.015 percent or less, no increase in the NSPS is provided; for a fuel-bound nitrogen concentration of 0.03 percent, the NSPS is increased by 0.0012 percent or 12 parts per million (ppm). The NSPS  $\text{NO}_x$  emission limit adjustment is not affected by natural gas combustion.

## B.2 BEST AVAILABLE CONTROL TECHNOLOGY

The "top-down" analysis for determining BACT, as provided for in EPA's Draft 1990 New Source Review Workshop Manual, is used by the FDEP in determining BACT under Rule 62-212.400(5)(c) F.A.C. The procedure involves 5 steps: identification of control technologies, elimination of technically infeasible control technologies, a ranking of the control technologies, an evaluation of the effective control technologies and the selection of BACT.

The identification of control technologies is developed from the information obtained from BACT/LAER Information System (BLIS) database maintained at EPA's National Computer Center located at Research Triangle Park, North Carolina. While these data are comprehensive it is often not up to date with the most recent BACT/LAER decisions and separate contact with state agencies is required. LAER is distinctly different from BACT in that there is no consideration of economic, energy, or environmental impacts; if a control technology has previously been installed, it must be required as LAER. LAER is defined as follows:

Lowest achievable emission rate means, for any source, the more stringent rate of emissions based on the following: (i) The most stringent emissions limitation which is contained in the implementation plan of any State of such class or category of stationary source, unless the owner or operator of the proposed stationary source demonstrates that such limitations are not achievable; or (ii) The most stringent emissions limitation which is achieved in practice by such class or category of stationary source. This limitation, when applied to a modification, means the lowest achievable emissions rate for the new or modified emissions units within the stationary source. In no event shall the application of this term permit a proposed new modified stationary source to emit any pollutant in excess of the amount allowable under applicable new source standards of performance (40 CFR 51, Appendix S.II, A.18).

The elimination of infeasible technologies is based on those engineering aspects that would preclude a technology's use due to physical, chemical or other engineering consideration. Control technologies that are technically feasible are ranked by control effectiveness, with determination of the environmental, economic and energy costs and benefits of the control technologies. This information forms the basis for the case-by-case consideration of environmental, energy and economic impacts. The "top" feasible control alterable is selected

unless it can be rejected based on economic, environmental or energy considerations. This section of Appendix B presents information related to the proposed BACT emission limitation.

### **B.2.1 NITROGEN OXIDES**

NO<sub>x</sub> emissions from combustion of fossil fuels consist of thermal NO<sub>x</sub> and fuel-bound NO<sub>x</sub>. Thermal NO<sub>x</sub> is formed from the reaction of oxygen and nitrogen in the combustion air at combustion temperatures. Formation of thermal NO<sub>x</sub> depends on the flame temperature, residence time, combustion pressure, and air-to-fuel ratios in the primary combustion zone. The design and operation of the combustion chamber dictates these conditions. Fuel-bound NO<sub>x</sub> is created by the oxidation of volatilized nitrogen in the fuel. Nitrogen content in the fuel is the primary factor in its formation.

#### **Identification of NO<sub>x</sub> Control Technologies**

Table B-2 presents a listing of the lowest achievable emission rates/best available control technology (LAER/BACT) decisions made by state environmental agencies and EPA regional offices for gas turbines. This table was developed from the information obtained from BACT/LAER Information System (BLIS) database maintained at EPA's National Computer Center located at Research Triangle Park, North Carolina.

Historically, the most stringent NO<sub>x</sub> controls for CTs established as LAER/BACT by state agencies were combustion controls with selective catalytic reduction (SCR) and combustion controls alone. SCR is a post-combustion control, while advanced dry low-NO<sub>x</sub> combustors minimize the formation of NO<sub>x</sub> in the combustion process. When SCR has been employed, wet injection and dry low-NO<sub>x</sub> combustion technology are used initially to reduce NO<sub>x</sub> emissions.

Wet injection was the first combustion technology introduced for combustion turbines (pre-1980's) and was the primary method of reducing NO<sub>x</sub> emissions from CTs prior to the 1990's. Indeed, this method of control was first mandated by the NSPS to reduce NO<sub>x</sub> levels to 75 parts per million by volume, dry (ppmvd) (corrected to 15 percent O<sub>2</sub> and heat rate).



Development of improved wet injection combustors reduced NO<sub>x</sub> concentrations to 25 ppmvd (corrected to 15 percent O<sub>2</sub>) when burning natural gas.

The dry low-NO<sub>x</sub> combustion technology has been developed and made available since the early 1990's for gas turbines to achieve emission levels of 25 ppmvd corrected to 15 percent O<sub>2</sub>. More recently, however, CT manufacturers have developed dry low-NO<sub>x</sub> combustors that can reduce NO<sub>x</sub> concentrations to 10 ppmvd (corrected to 15 percent O<sub>2</sub>) or less when firing natural gas.

SCR has been installed or permitted in over 100 projects. The majority of these projects (more than 90 percent) were initially cogeneration facilities with capacities of 50 MW or less. Many of these projects that have installed SCR have been in the Southern California NO<sub>2</sub> nonattainment area where SCR was initially required not as BACT but as LAER, a more stringent requirement. As noted previously, there are distinct regulatory and policy differences between LAER and BACT. As discussed in Section 3.0, BACT involves an evaluation of the economic, environmental, and energy impacts of alternative control technologies. In contrast, LAER only considers the technical aspects of control.

More recently, projects with SCR have been installed throughout the US including the states of Vermont, Massachusetts, Connecticut, New Jersey, New York, Rhode Island, Virginia, and Florida. A majority of these projects are also cogeneration facilities or independent power producers. The size of these projects ranges from 22 MW to over 500 MW. While almost all of the facilities have distillate oil as backup fuel, distillate oil generally is restricted by permit to 1,000 hours or less per CT.

Reported and permitted NO<sub>x</sub> removal efficiencies of SCR range from 40 to 80 percent of NO<sub>x</sub> in the exhaust gas stream. The most common emission limiting standards associated with SCR are 9 ppmvd corrected to 15 percent O<sub>2</sub> or less for natural gas firing.

Other available control technologies that have become available for controlling NO<sub>x</sub> emissions from combustion turbines for include SCONO<sub>x</sub><sup>™</sup> and XONON<sup>™</sup>. SCONO<sub>x</sub><sup>™</sup> is an add-on control using absorption and chemical conversion to remove NO<sub>x</sub> formed from combustion, while XONON<sup>™</sup> is a catalytic combustion system integral to the turbine. Other

potential technologies used in combustion process for NO<sub>x</sub> removal include: NO<sub>x</sub>OUT, Thermal DeNO<sub>x</sub>, and NSCR.

### Technology Descriptions and Feasibility

#### **Wet Injection**

The injection of water or steam in the combustion zone of CTs reduces the flame temperature with a corresponding decrease of NO<sub>x</sub> emissions. The amount of NO<sub>x</sub> reduction possible depends on the combustor design and the water-to-fuel ratio employed. An increase in the water-to-fuel ratio will cause a concomitant decrease in NO<sub>x</sub> emissions until flame instability occurs. At this point, operation of the CT becomes inefficient and unreliable, and significant increases in products of incomplete combustion results (i.e., CO and VOC emissions). In "F" Class turbines using wet injection with gas firing, the NO<sub>x</sub> emission rates in the 30 ppm have been demonstrated. However, wet injection is no longer offered for gas firing in "F" Class turbines. Wet injection is the only current feasible means of reducing NO<sub>x</sub> emissions in the combustion process when firing oil.

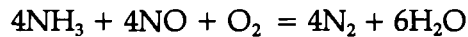
#### **Dry Low-NO<sub>x</sub> Combustor**

In the past several years, CT manufacturers have offered and installed machines with dry low-NO<sub>x</sub> combustors. These combustors, which are offered on conventional machines manufactured by General Electric (GE), Siemens/Westinghouse, and ABB, can achieve NO<sub>x</sub> concentrations of 25 ppmvd or less when firing natural gas. GE and Siemens/Westinghouse have offered dry low-NO<sub>x</sub> combustors on advanced heavy-duty industrial machines. Thermal NO<sub>x</sub> formation is inhibited by using combustion techniques where the natural gas and combustion air are premixed before ignition. For the CT being considered for the Project, the combustion chamber design includes the use of dry low-NO<sub>x</sub> combustor technology. The NO<sub>x</sub> emission level when firing natural gas at baseload conditions is 10 ppmvd (corrected to 15 percent O<sub>2</sub>), a level which is guaranteed by the selected vendor (GE) for the Project.

#### **Selective Catalytic Reduction (SCR)**

Selective Catalytic Reduction (SCR) uses ammonia (NH<sub>3</sub>) to react with NO<sub>x</sub> in the gas stream in the presence of a catalyst. NH<sub>3</sub>, which is diluted with air to about 5 percent by volume, is

introduced into the gas stream at reaction temperatures between 600°F and 750°F. The reactions are as follows:



SCR operating experience, as applied to gas turbines, consists primarily of baseload natural-gas-fired installations either of cogeneration or combined-cycle configuration. Exhaust gas temperatures of simple-cycle CTs generally are in the range of 1,000°F to 1,200°F, which exceeds the optimum range for SCR with base metal catalysts. All current SCR applications have the catalyst placed in the HRSG to achieve proper reaction conditions. This allows a relatively constant temperature for the reaction of  $\text{NH}_3$  and  $\text{NO}_x$  on the catalyst surface.

The use of SCR has been primarily limited to combined-cycle facilities that burn natural gas with small amounts of fuel oil. Traditional metal SCR catalysts were contaminated by sulfur-containing fuels. For most fuel-oil-burning facilities, catalyst operation was discontinued, or the exhaust bypasses the SCR system. This was due to the formation of ammonium salts (ammonium sulfate and bisulfate) resulting from the reaction of  $\text{NH}_3$  and sulfur combustion products. Ammonium bisulfate can be corrosive and could cause damage to the HRSG surfaces that follow the catalyst, as well as to the stack. Corrosion protection for these areas would be required with concomitant cost and technical requirements. Ammonium sulfate is emitted as particulate matter. While the formation of ammonium salts is primarily associated with oil firing, sulfur combustion products from natural gas also could form small amounts of ammonium salts. Ceramic and specially designed catalysts have been designed to overcome the problems with base-metal catalysts. The sulfur in No. 2 distillate oil has also been reduced from 0.5 percent available in the early 1990's to 0.05 percent. In addition, HRSG designs can accommodate the impacts of the formation of ammonium salts.

For simple-cycle combustion turbines, SCR has had limited applications. Zeolite and specially designed high temperature catalysts, which are reported to be capable of withstanding temperature ranges up to 1,050°F, have become commercially available. Their initial application with SCR has primarily been limited to applications on internal combustion engines. The initial optimum performance of an SCR system using a zeolite

catalyst is reported to range from about 800°F to 900°F. Recently, SCR vendors have offered high temperature catalysts for simple-cycle applications up to 1,050°F. At temperatures of 1,100°F and above, the high-temperature catalyst will be irreparably damaged.

In the 1990s there are four simple-cycle combustion turbine projects that have installed SCR with operating experience. These projects are:

- Redding Municipal Power – 3 GE Frame 5 CTs fired with natural gas. The CTs are operated as a peaking facility.
- SoCal Gas Company – 4 Solar Centaur CTs (4MW equivalent each) fired with natural gas. The CTs are operated in intermediate cycling duty.
- UnoCal Brea Research Center – a single 4 MW CT firing natural gas. The CT operates in intermediate to base load duty.
- Puerto Rico Electric Power Authority (Cambalache Facility) – 3 ABB Type 11 N (83 MW each) firing No. 2 distillate oil.

The SCRs for all these CTs were designed to operate at temperatures less than 1,000°F. Many of the smaller CTs have exhaust temperatures less than 1,000°F. The Cambalache Facility had a once through steam generator in the ductwork leading to SCR used for power augmentation that reduced the catalyst temperature to less than 1,000°F. Experience on these systems has shown significant catalyst deactivation occurs with peaking and intermediate cycling duty while firing natural gas. Under these conditions catalyst deactivation has occurred after operating from 350 to 4,000 hours. For intermediate-base load duty and firing natural gas, catalyst deactivation improved but still occurred after 8,000 hour of operation and well less the catalyst guarantee. When firing distillate oil, catalyst deactivation occurred after 600 hours. Due to the problems with oil firing, the SCR system for the Cambalache Facility has been removed.

The "F" Class turbines have higher exhaust temperatures and would require exhaust temperature reduction for the technology to be feasible. There are no current applications of SCR on "F" Class combustion turbines. The experience with SCR on simple-cycle turbines suggests the technology is available from vendors but has not been demonstrated as technically feasible.

**SCONO<sub>x</sub>™ Process**

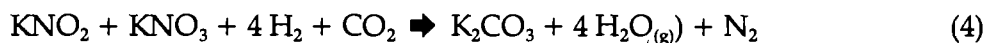
SCONO<sub>x</sub>™ is a NO<sub>x</sub> and CO control system exclusively offered by Goal Line Environmental Technologies (GLET). GLET is a partnership formed by Sunlaw Energy Corporation and Advanced Catalyst Systems, Inc. In 1998, ABB acquired the exclusive license for the technology in the United States for control applications larger than 100 MW.

The SCONO<sub>x</sub>™ system employs a single catalyst to simultaneously oxidize CO to CO<sub>2</sub> and NO to NO<sub>2</sub>. NO<sub>2</sub> formed by the oxidation of NO is subsequently absorbed onto the catalyst surface through the use of a potassium carbonate absorber coating. The SCONO<sub>x</sub>™ oxidation/absorption cycle reactions are:



CO<sub>2</sub> produced by reaction (1) and (2) is released to the atmosphere as part of the CT/HRSG exhaust gas stream.

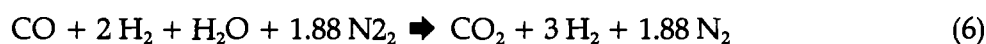
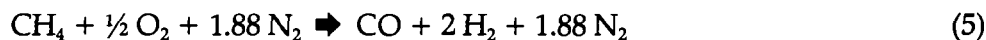
As shown in Reaction (3), the potassium carbonate catalyst coating reacts with NO<sub>2</sub> to form potassium nitrites and nitrates. Prior to saturation of the potassium carbonate coating, the catalyst must be regenerated. This regeneration is accomplished by passing a dilute hydrogen-reducing gas across the surface of the catalyst in the absence of O<sub>2</sub>. Hydrogen in the reducing gas reacts with the nitrites and nitrates to form water and elemental nitrogen. CO<sub>2</sub> in the regeneration gas reacts with potassium nitrites and nitrates to form potassium carbonate; this compound is the catalyst absorber coating present on the surface of the catalyst at the start of the oxidation/absorption cycle. The SCONO<sub>x</sub>™ regeneration cycle reaction is:



Water vapor and elemental nitrogen are released to the atmosphere as part of the CT/HRSG exhaust stream. Following regeneration, the SCONO<sub>x</sub><sup>™</sup> catalyst has a fresh coating of potassium carbonate, allowing the oxidation/absorption cycle to begin again. There is no net gain or loss of potassium carbonate after both the oxidation/absorption and regeneration cycles have been completed.

Since the regeneration cycle must take place in an oxygen-free environment, the section of catalyst undergoing regeneration is isolated from the exhaust gas stream using a set of louvers. Each catalyst section is equipped with a set of upstream and downstream louvers. During the regeneration cycle, these louvers close and valves open allowing fresh regeneration gas to enter and spent regeneration gas to exit the catalyst section being regenerated. At any given time, 75 percent of the catalyst sections will be in the oxidation/absorption cycle, while 25 percent will be in regeneration mode. A regeneration cycle is typically set to last for 3 to 5 minutes.

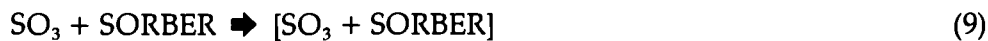
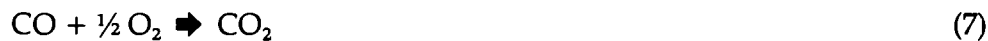
Regeneration gas is produced by reacting natural gas with O<sub>2</sub> present in ambient air. The SCONO<sub>x</sub><sup>™</sup> system uses a gas generator produced by Surface Combustion. This unit uses a two-stage process to produce hydrogen and carbon dioxide. In the first stage, natural gas and ambient air are reacted across a partial oxidation catalyst at 1,900°F to form CO and hydrogen. Steam is added and the gas mixture is then passed across a low temperature shift catalyst, forming CO<sub>2</sub> and additional hydrogen. The resulting gas stream is diluted to less than 4 percent hydrogen using steam or another inert gas. The regeneration gas reactions are:



The SCONO<sub>x</sub><sup>™</sup> operates at a temperature range of 300 to 700°F and, therefore, must be installed in the appropriate temperature section of a HRSG. For SCONO<sub>x</sub><sup>™</sup> systems installed

in locations of the HRSG above 500°F, a separate regeneration gas generator is not required. Instead, regeneration gas is produced by introducing natural gas directly across the  $\text{SCONO}_x^{\text{TM}}$  catalyst that reforms the natural gas.

The  $\text{SCONO}_x^{\text{TM}}$  system catalyst is subject to reduced performance and deactivation due to exposure to sulfur oxides. For this reason, an additional catalytic oxidation/absorption system ( $\text{SCONO}_x^{\text{TM}}$ ) to remove sulfur compounds is installed upstream of the  $\text{SCONO}_x^{\text{TM}}$  catalyst. During regeneration of the  $\text{SCONO}_x^{\text{TM}}$  catalyst, either hydrogen sulfide or  $\text{SO}_2$  is released to the atmosphere as part of the CT/HRSG exhaust gas stream. The absorption portion of the  $\text{SCONO}_x^{\text{TM}}$  process is proprietary.  $\text{SCONO}_x^{\text{TM}}$  oxidation/absorption and regeneration reactions are:



Utility materials needed for the operation of the  $\text{SCONO}_x^{\text{TM}}$  control system include ambient air, natural gas, water, steam, and electricity. The primary utility material is natural gas used for regeneration gas production. Steam is used as the carrier/dilution gas for the regeneration gas. Electricity is required to operate the computer control system, control valves, and louver actuators.

Commercial experience to date with the  $\text{SCONO}_x^{\text{TM}}$  control system is limited to one small combined-cycle (CC) power plant located in Los Angeles. This power plant, owned by GLET partner Sunlaw Energy Corporation, utilizes a GE LM2500 turbine (30 MW size) equipped with water injection to control  $\text{NO}_x$  emissions to approximately 25 ppmvd. The  $\text{SCONO}_x^{\text{TM}}$  control system was installed at the Sunlaw Energy facility in December 1996 and has achieved a  $\text{NO}_x$  exhaust concentration of 3.5 ppmv resulting in an approximate 85 percent  $\text{NO}_x$  removal efficiency.

The SCONO<sub>x</sub>™ control technology is not considered to be technically feasible because it has not been commercially demonstrated on large CTs. The CTs planned for the Project, GE Frame 7F units, each have a nominal generating capacity of 174 MW which are approximately seven times larger than the nominal 25-MW GE LM2500 utilized at the Sunlaw Energy Corporation Los Angeles facility. Technical problems associated with scale-up of the SCONO<sub>x</sub>™ technology given the large differences in machine flow rates are unknown. Additional concerns with the SCONO<sub>x</sub>™ control technology include process complexity (multiple catalytic oxidation / absorption / regeneration systems), reliance on only one supplier, and the relatively brief operating history of the technology.

#### **XONON™ Catalytic Combustor**

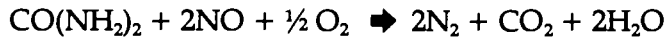
Catalytic combustors are being developed for low emission applications on turbines where the catalyst is internal to the combustion system. The XONON™ Combustion System is a catalytic combustion system developed by Catalytica Combustion Systems, Inc. that can achieve low emission levels of NO<sub>x</sub>, CO and VOCs. The XONON™ system combusts the fuel over a catalyst, reducing the temperature of combustion and providing for more complete combustion of the fuel. The system is referred to as "flameless combustion" where temperatures are below those where limited NO<sub>x</sub> formation occurs. However, the exhaust temperatures from a combustion turbine standpoint are still sufficient for the expansion of the gases through the turbine for power generation. Emission levels of NO<sub>x</sub> at less than 2 ppm have been reported for the 1.5 MW Kawasaki gas turbine located at Sun Valley Power. Recently, this technology has been proposed for a 750 MW combined-cycle facility. This facility, the Pastoria Energy Facility, is a project proposed by affiliates of Enron Corporation, which has a 15 percent interest in Catalytica Combustion Systems, Inc. Commercial operation is scheduled for the summer of 2003. Catalytica is currently working in collaboration with several gas turbine manufacturers including General Electric, Pratt & Whitney, Rolls Royce Allison and Solar.

#### **NO<sub>x</sub>OUT Process**

The NO<sub>x</sub>OUT process originated from the initial research by the Electric Power Research Institute (EPRI) in 1976 on the use of urea to reduce NO<sub>x</sub>. EPRI licensed the proprietary process to Fuel Tech, Inc., for commercialization. In the NO<sub>x</sub>OUT process, aqueous urea is



injected into the flue gas stream ideally within a temperature range of 1,600°F to 1,900°F. In the presence of oxygen, the following reaction results:



The amount of urea required is most cost-effective when the treatment rate is 0.5 to 2 moles of urea per mole of  $\text{NO}_x$ . In addition to the original EPRI urea patents, Fuel Tech claims to have a number of proprietary catalysts capable of expanding the effective temperature range of the reaction to between 1,600°F and 1,950°F. Advantages of the system are as follows:

1. Low capital and operating costs as a result of use of urea injection, and
2. The proprietary catalysts used are nontoxic and nonhazardous, thus eliminating potential disposal problems.

Disadvantages of the system are as follows:

1. Formation of ammonia from excess urea treatment rates and/or improper use of reagent catalysts, and
2. Sulfur trioxide ( $\text{SO}_3$ ), if present, will react with ammonia created from the urea to form ammonium bisulfate, potentially plugging the cold end equipment downstream.

Commercial application of the  $\text{NO}_x$ OUT system is limited and the  $\text{NO}_x$ OUT system has not been demonstrated on any combustion turbine/HRSG unit.

The  $\text{NO}_x$ OUT process is not technically feasible for the proposed Project because of the high application temperature of 1,600°F to 1,950°F. The maximum exhaust gas temperature of the project CT is about 1,100°F. Raising the exhaust temperature the required amount essentially would require installation of a heater. This would be economically prohibitive and would result in an increase in fuel consumption, an increase in the volume of gases that must be treated by the control system, and an increase in uncontrolled air emissions, including  $\text{NO}_x$ .

**Thermal DeNO<sub>x</sub>**

Thermal DeNO<sub>x</sub> is Exxon Research and Engineering Company's patented process for NO<sub>x</sub> reduction. The process is a high temperature selective noncatalytic reduction (SNCR) of NO<sub>x</sub> using ammonia as the reducing agent. Thermal DeNO<sub>x</sub> requires the exhaust gas temperature to be above 1,800°F. However, use of ammonia plus hydrogen lowers the temperature requirement to about 1,000°F. For some applications, this must be achieved by additional firing in the exhaust stream before ammonia injection.

The only known commercial applications of Thermal DeNO<sub>x</sub> are on heavy industrial boilers, large furnaces, and incinerators that consistently produce exhaust gas temperatures above 1,800°F. There are no known applications on or experience with CTs. Temperatures of 1,800°F require alloy materials constructed with very large piping and components since the exhaust gas volume would be increased by several times. As with the NO<sub>x</sub>OUT process, high capital, operating, and maintenance costs are expected because of material requirements, an additional duct burner system, and fuel consumption. Uncontrolled emissions would increase because of the additional fuel burning.

Thus, the Thermal DeNO<sub>x</sub> process will not be considered for the proposed Project since its high application temperature makes it technically infeasible. The maximum exhaust gas temperature of the Project combustion turbine is typically 1,100°F; the cost to raise the exhaust gas to such a high temperature is prohibitively expensive.

**Nonselective Catalytic Reduction**

Certain manufacturers, such as Engelhard, market a nonselective catalytic reduction system (NSCR) for NO<sub>x</sub> control on reciprocating engines. The NSCR process requires a low oxygen content in the exhaust gas stream and high temperature (700°F to 1,400°F) in order to be effective. CTs have the required temperature but also have high oxygen levels (greater than 12 percent) and, therefore, cannot use the NSCR process. As a result, NSCR is not a technically feasible add-on NO<sub>x</sub> control device for CTs.

### Technology Demonstration and Feasibility

The combustion technologies of dry low-NO combustors and wet injection are available, demonstrated and technically feasible for combustion turbines in simple-cycle configuration. The advanced dry low-NO<sub>x</sub> combustion technology alone can achieve 10 ppm (corrected to 15 percent O<sub>2</sub> dry conditions) when firing natural gas and water injection is capable of achieving a NO<sub>x</sub> emission level of 42 ppm when firing natural gas (corrected to 15 percent O<sub>2</sub> dry conditions). Wet injection cannot achieve emission rates lower than 42 ppm when firing natural gas in an "F" Class machine and is not offered by the preferred vendor (i.e., GE). Injection of larger amounts of water than recommended by the manufacture will potential damage the machine.

The technical evaluation of post-combustion gas controls that include NO<sub>x</sub>OUT, Thermal DeNO<sub>x</sub>, and NSCR, and indicate that these processes have not been applied to either simple-cycle or combined-cycle combustion turbines and are technically infeasible for the Project because of process constraints (e.g., temperature). SCONO<sub>x</sub><sup>™</sup> is potentially feasible for combined-cycle turbines but is infeasible for simple-cycle operation. There is currently no commercially demonstrated application of SCONO<sub>x</sub><sup>™</sup> in a large combined-cycle unit (i.e., 170 MW). While the XONON<sup>™</sup> catalytic combustion system can be applied to both simple-cycle and combined-cycle, application to a large combined-cycle unit has also not been demonstrated. For these reasons, the SCONO<sub>x</sub><sup>™</sup> and XONON<sup>™</sup> are still considered in the commercial demonstration stage. SCR is commercially available, technically feasible and demonstrated for combined-cycle units. While high-temperature "hot" SCR is feasible, it has not been demonstrated on simple-cycle "F" class turbines in peaking service.

For simple-cycle operation, dry low-NO<sub>x</sub> combustion technology and water injection in combination with SCR are available from vendors but the technical feasibility of SCR is questionable.

Below is a summary of the technical availability, demonstration and feasibility for the proposed Project.

Simple-cycle:

<u>Technology</u>	<u>Status</u>
Selective Catalytic Reduction	Available, Not Demonstrated and Potentially Feasible
Dry Low-NO <sub>x</sub> Combustors	Available, Demonstrated and Feasible for Gas Firing
Wet Injection	Available, Demonstrated and Feasible for Oil Firing
SCO NO <sub>x</sub>	Not Available or Feasible
XOXON™	Not Yet Demonstrated, Potentially Feasible
Thermal De NO <sub>x</sub>	Not Available or Feasible
NO <sub>x</sub> Out	Not Available or Feasible
NSCR	Not Available or Feasible

### SCR Cost Estimates

Tables B-3 and B-4 present the total capital and annualized cost for SCR applied to simple-cycle operation, respectively. The costs were developed using the EPA Cost Control Manual (EPA, 1990 & 1993). Vendor based estimates were used for the SCR system. Standard EPA recommended cost factors were used. A capital recovery period of 15 years was used for the capital costs.

### Comparison of Economic, Environmental, and Energy Impacts

Table B-5 presents a comparison of the economic, environmental, and energy impacts associated with the top control alternatives for the simple-cycle unit. Table B-6 presents the potential emissions resulting from the formation of ammonium salts (i.e., particulate matter), ammonia slip and secondary emissions. The latter results from generation lost due to the back pressure of the SCR system.

## **B.2.2 CARBON MONOXIDE**

### Identification of CO Control Technologies

CO emissions are a result of incomplete or partial combustion of fossil fuel. Combustion design and catalytic oxidation are the control alternatives that are viable for the Project. Table B-7 presents a listing of LAER/BACT decisions for CO emissions from combustion

turbines. Combustion design is the more common control technique used in CTs. Sufficient time, temperature, and turbulence is required within the combustion zone to maximize combustion efficiency and minimize the emissions of CO. Combustion efficiency is dependent upon combustor design. For the CTs being evaluated, CO emissions will not exceed 12 ppmvd, corrected to 15 percent O<sub>2</sub>, dry conditions when firing natural gas under full load conditions and 20 ppmvd, corrected to 15 percent O<sub>2</sub>, dry conditions when firing distillate oil under full load conditions.

Catalytic oxidation is a post-combustion control that has been employed in CO nonattainment areas where regulations have required CO emission levels to be less than those associated with wet injection. These installations have been required to use LAER technology and typically have CO limits in the 10 ppm range (corrected to dry conditions) and less.

#### Technology Description

In an oxidation catalyst control system, CO emissions are reduced by allowing unburned CO to react with oxygen at the surface of a precious metal catalyst, such as platinum. Combustion of CO starts at about 300°F, with efficiencies above 90 percent occurring at temperatures above 600°F. Catalytic oxidation occurs at temperatures 50 percent lower than that of thermal oxidation, which reduces the amount of thermal energy required.

For CTs, the oxidation catalyst can be located directly after the CT. Catalyst size depends upon the exhaust flow, temperature, and desired efficiency. The existing oxidation catalyst applications primarily have been limited to smaller cogeneration facilities burning natural gas. Oxidation catalysts have not been used on fuel-oil-fired CTs. The use of sulfur-containing fuels in an oxidation catalyst system would result in an increase of SO<sub>3</sub> emissions and concomitant corrosive effects to the stack. In addition, trace metals in the fuel could result in catalyst poisoning during prolonged periods of operation.

During simple-cycle operation the units likely will require numerous startups and experience variations in exhaust conditions that will influence catalyst life and performance. Very little technical data exist to demonstrate the effect of such cycling.

### Oxidation Catalyst Costs

Tables B-8 and B-9 present the capital and annualized cost for an oxidation catalyst applied to simple-cycle operation. The maximum CO impacts are less than 0.1 percent of the applicable ambient air quality standards. There would also be no secondary benefits, such as reducing acidic deposition, to reducing CO.

### Comparison of Economic, Environmental, and Energy Impacts

Table B-10 presents a comparison of the economic, environmental, and energy impacts associated with the top control alternatives for the combined-cycle unit. Table B-11 presents the potential emissions resulting from the formation of ammonium salts (i.e., particulate matter), ammonia slip and secondary emissions. The latter results from generation lost due to the back pressure of the oxidation catalyst.

Table B-1. Federal NSPS for Electric Utility Stationary Gas Turbines

Pollutant	Emission Limitation <sup>a</sup>
Nitrogen Oxides <sup>b</sup>	0.0075 percent by volume (75 ppm) at 15 percent O <sub>2</sub> on a dry basis adjusted for heat rate and fuel nitrogen

<sup>a</sup> Applicable to electric utility gas turbines with a heat input at peak load of greater than 100 x 10<sup>6</sup> Btu/hr.

<sup>b</sup> Standard is multiplied by 14.4/Y; where Y is the manufacturer's rated heat rate in kilojoules per watt at rated load or actual measured heat rate based on the lower heating value of fuel measured at actual peak load; Y cannot be greater than 14.4. Standard is adjusted upward (additive) by the percent of nitrogen in the fuel:

Fuel-Bound Nitrogen (percent by weight)	Allowed Increase NO <sub>x</sub> Percent by Volume
$N \leq 0.015$	0
$0.015 < N \leq 0.1$	0.04(N)
$0.1 < N \leq 0.25$	$0.004 + 0.0067(N - 0.1)$
$N > 0.25$	0.005

where: N = the nitrogen content of the fuel (percent by weight).

Source: 40 CFR 60 Subpart GG.

Table B-2. Summary of Best Available Control Technology (BACT) Determinations for Nitrogen Oxide (NO<sub>x</sub>) Emissions for Combustion Turbines

Facility Name	State	Permit Number	Permit Issue Date	Unit/Process Description	Capacity (size)	NO <sub>x</sub> Emission Limit	Control Method	Basis
KISSIMMEE UTILITIES AUTHORITY	FL	PSD-FL-254	12/16/99	TURBINE, COMBUSTION	250.00 MW	9.0000 PPMVD	GE DLN2.6	BACT-PSD
DUKE ENERGY NEW SOMERVA BEACH POWER CO. LP	FL	PSD-FL-257	10/15/99	TURBINE-GAS, COMBINED CYCLE	500.00 MW (2 UNITS)	9.0000 PPM @ 15% O2	DLN	BACT-PSD
TAMPA ELECTRIC COMPANY (TEC)	FL	PSD-FL-263	10/15/99	TURBINE, COMBUSTION, SIMPLE CYCLE	165.00 MW	10.5000 PPM @ 15% O2	DLN	BACT-PSD
CLEANDER POWER PROJECT	FL	PSD-FL-258	10/1/99	TURBINE-GAS, COMBINED CYCLE	190.00 MW	9.0000 PPM @ 15% O2	DLN 2.6	BACT-PSD
PDC EL PASO MILFORD LLC	CT	105-0068	4/16/99	TURBINE, COMBUSTION, ABB GT-24, #1 WITH 2 CHILLERS	1.97 MMCF/H	2.0000 PPMV @ 15% O2 GAS	SCR WITH AMMONIA INJECTION	LAER
PDC EL PASO MILFORD LLC	CT	105-0069	4/16/99	TURBINE, COMBUSTION, ABB GT-24E, #2 WITH 2 CHILLERS	1.97 MMCF/H	2.0000 PPMV @ 15% O2 GAS	SCR WITH AMMONIA INJECTION	LAER
ALABAMA POWER COMPANY - THEODORE COGENERATION	AL	503-8073	3/16/99	TURBINE, WITH DUCT BURNER	170.00 MW	0.0130 LB/MMBTU	DLN COMBUSTOR IN CT, LNB IN DUCT BURNER, SCR	BACT-PSD
WYANDOTTE ENERGY	MI	279-98	2/8/99	TURBINE, COMBINED CYCLE, POWER PLANT	500.00 MW	4.5000 PPM	SCR	BACT
MOBILE ENERGY LLC	AL	503-8066	1/5/99	TURBINE, GAS, COMBINED CYCLE	168.00 MW	0.0190 LB/MMBTU	SCR & DLN COMBUSTORS DURING GAS FIRING.	BACT-PSD
COLORADO SPRINGS UTILITIES	CO	0410030	1/4/99	TURBINE, COMBINE, NATURAL GAS FIRED	30.00 MW EACH	15.0000 PPMVD ABOVE 70% LOAD	POLLUTION PREVENTION BUILT INTO EQUIPMENT.	BACT-PSD
TENUSKA GEORGIA PARTNERS, L.P.	GA	4-11-149-0004-P-01-0	12/18/98	TURBINE, COMBUSTION, SIMPLE CYCLE, 6	160.00 MW EA	15.0000 PPMVD @ 15% O2	USING 15% EXCESS AIR. NOX EMISSION IS BECAUSE OF NATURAL GAS.	BACT-PSD
TENUSKA GEORGIA PARTNERS, L.P.	GA	4-11-149-0004-P-01-0	12/18/98	TURBINE, COMBUSTION, SIMPLE CYCLE, 6	160.00 MW EA	42.0000 PPMVD @ 15% O2	USING 15% EXCESS AIR. NOX EMISSION IS BECAUSE OF FUEL OIL.	BACT-PSD
WESTBROOK POWER LLC	ME	A-743-71-A-N	12/4/98	TURBINE, COMBINED CYCLE, TWO	528.00 MW TOTAL	2.5000 PPM @ 15% O2	SELECTIVE CATALYTIC REDUCTION AND DRY LOW NOX BURNERS.	LAER
GORHAM ENERGY LIMITED PARTNERSHIP	ME	A-735	12/4/98	TURBINE, COMBINED CYCLE	900.00 MW TOTAL	2.5000 PPM @ 15% O2 (NAT G)	SELECTIVE CATALYTIC REDUCTION.	LAER
SANTA ROSA ENERGY LLC	FL	PSD-FL 253	12/4/98	TURBINE, COMBUSTION, NATURAL GAS	241.00 MW	9.8000 PPMVD @ 15% O2 DB ON	DRY LOW NOX BURNER	BACT-PSD
LSP - COTTAGE GROVE, L.P.	MN	16300087-001	11/10/98	GENERATOR, COMBUSTION TURBINE & DUCT BURNER	1988.00 MMBTU/H (CTG)	4.5000 PPMVD @ 15% O2 (NG)	SELECTIVE CATALYTIC REDUCTION (SCR) WITH A NOX CEM AND A NOX PEM.	BACT-PSD
CHAMPION INTERNATL. CORP. & CHAMP. CLEANENERGY	ME	A-22-71-N-A	9/14/98	TURBINE, COMBINED CYCLE, NATURAL GAS	175.00 MW	9.0000 PPMVD @ 15% O2 GAS	DRY LOW NOX BURNER	BACT-OTHER
ALABAMA POWER PLANT BARRY	AL	503-1001	8/7/98	TURBINES, COMBUSTION, NATURAL GAS	510.00 MW(TOTAL)	0.0130 LB/MMBTU	NATURAL GAS, CT-DLN COMBUSTORS, DUCTBURNER, LOW NOX BURNER, COMBINED STACK SCR	BACT-PSD
TNP TECH. LLC (FORMERLY TX-NM POWER CO.)	NM	PSD-NM-90-M2	8/7/98	GAS TURBINES	375.00 MMBTU/H	15.0000 PPM	WATER INJECTION FOLLOWED BY SELECTIVE CATALYTIC REDUCTION (SCR)	BACT-PSD
CASCO RAY ENERGY CO	ME	A-728	7/13/98	TURBINE, COMBINED CYCLE, NATURAL GAS, TWO	170.00 MW EACH	3.5000 PPM @ 15% O2	SELECTIVE CATALYTIC REDUCTION	BACT-PSD
CITY OF LAKEBLAND ELECTRIC AND WATER UTILITIES	FL	PSD-FL-245	7/10/98	TURBINE, COMBUSTION, GAS FIRED W/FUEL OIL ALSO	2174.00 MMBTU/H	25.0000 PPM @ 15% O2	DRY LOW NOX BURNERS FOR SIMPLE CYCLE, SCR WHEN COMBINED CYCLE	BACT-PSD
COLORADO SPRINGS UTILITIES-NIXON POWER PLANT	CO	94EP132	6/30/98	SIMPLE CYCLE TURBINE, NATURAL GAS	1122.00 MM BTU/HR	25.0000 PPM @ 15% O2	DRY LOW NOX COMBUSTION	BACT-PSD
BRIDGEPORT ENERGY, LLC	CT	0150190 & 0150191	6/29/98	TURBINES, COMBUSTION MODEL V84.3A, 2 SIEMES	260.00 MW/HRSG PER TURBINE	6.0000 PPM NAT. GAS	900.00 MW/HRSG PER TURBINE	BACT-PSD
CITY OF TALLAHASSEE UTILITY SERVICES	FL	PSD-FL-239	5/29/98	TURBINE, COMBINED CYCLE, MULTIPLE FUELS	1468.00 MMBTU/H	0.0000 SEE P2 DESCRIPTION	DLN BURNERS VERSION 2.6 BY GE	BACT-OTHER
GENERAL ELECTRIC PLASTICS	AL	207-0008-X016	5/27/98	COMBINED CYCLE (TURBINE AND DUCT BURNER)	0.00	0.0700 LBS/MMBTU COMBINED	DRY LOW NOX BURNER ON TURBINE AND LOW NOX BURNER ON DUCT BURNER	BACT-PSD
RUMFORD POWER ASSOCIATES	ME	A-724-71-A-N	5/1/98	TURBINE GENERATOR, COMBUSTION, NATURAL GAS	1906.00 MMBTU/H	3.5000 PPM @ 15% O2	SCR AMMONIA INJECTION SYSTEM AND CATALYTIC REACTOR TO REDUCE NOX.	BACT-PSD
ANDROSOGGIN ENERGY LIMITED	ME	A-718-71-A-N	3/31/98	GAS TURBINES, COGEN, W/DUCT BURNERS	675.00 MMBTU/H TURBINE	6.0000 PPM @ 15% O2 NG	LOW NOX BURNERS. LOW NOX COMBUSTORS. SCR DURING GAS FIRING ONLY.	BACT-PSD
ANDROSOGGIN ENERGY LIMITED	ME	A-718-71-A-N	3/31/98	GAS TURBINES, COGEN, W/DUCT BURNERS	675.00 MMBTU/H TURBINE	42.0000 PPM @ 15% O2 NG OIL	LOW NOX COMBUSTORS, LOW NOX BURNERS, WATER INJECTION DURING OIL FIRING.	BACT-PSD
STAR ENTERPRISE	DE	APC-97/0503-CONST.(LAER)(NSPS)	3/30/98	TURBINES, COMBINED CYCLE, 2	826.60 MMBTU/H	16.0000 PPM @ 15% O2 SYN GAS	NITROGEN INJECTION WHILE FIRING SYNGAS AND STEAM INJECTION WHILE FIRING LSDF	LAER
STAR ENTERPRISE	DE	APC-97/0503-CONST.(LAER)(NSPS)	3/30/98	TURBINES, COMBINED CYCLE, 2	826.60 MMBTU/H	42.0000 PPM @ 15% O2 DIESEL	NITROGEN INJECTION WHILE FIRING SYNGAS AND STEAM INJECTION WHILE FIRING LSDF	LAER
SOUTHERN NATURAL GAS	AL	412-0013-X001 AND -X002	3/4/98	2-9160 HP GE MODEL M53002G NATURAL GAS TURBINES	9160.00 HP	53.0000 LB/HR		BACT-PSD
SOUTHERN NATURAL GAS	AL	206-0021-X001 AND -X002	3/2/98	9160 HP GE MODEL M53002G NATURAL GAS FIRED TURBINE	9160.00 HP	53.0000 LB/HR		BACT-PSD
TWO BLK GENERATION PARTNERS, LIMITED PARTNERSHIP	WY	CT-1352	2/27/98	TURBINE, STATIONARY	33.30 MW	25.0000 PPM @ 15% O2	DRY LOW NOX BURNERS	BACT-PSD
AIR LIQUIDE AMERICA CORPORATION	LA	PSD-LA-622	2/13/98	TURBINE GAS, GE, 7ME 7	966.00 MMBTU/H	9.0000 PPMV	DRY LOW NOX TO LIMIT NOX EMISSION TO 9PPMV	BACT-PSD
TIVERTON POWER ASSOCIATES	RI	RI-PSD-5	2/13/98	COMBUSTION TURBINE, NATURAL GAS	265.00 MW	3.5000 PPM @ 15% O2	SCR	LAER
MILLENNIUM POWER PARTNER, LP	MA	130921	2/2/98	TURBINE, COMBUSTION, WESTINGHOUSE MODEL 501G	2534.00 MMBTU/H	0.0130 LB/MMBTU	DRY LOW-NOX COMBUSTION TECHNOLOGY IN CONJUNCTION WITH SCR ADD-ON NOX CONTROLS.	BACT-PSD
BA5F CORPORATION	LA	PSD-LA-613	12/30/97	TURBINE, COGEN UNIT 2, GE FRAME 6	42.40 MW	8.0000 PPMV NAT. GAS	STEAM INJECTION AND SCR TO LIMIT NOX TO 8 PPM FOR NATURAL GAS AND 25 PPM FOR WASTE GAS (80% H2)	BACT-PSD
ALABAMA POWER COMPANY	AL	108-0018-X001 AND -X002	12/17/97	COMBUSTION TURBINE W/ DUCT BURNER (COMBINED CYCLE)	100.00 MW	15.0000 PPM	DRY LOW NOX BURNERS	BACT-PSD
BUCKNELL UNIVERSITY	PA	60-0001A	11/26/97	NG FIRED TURBINE, SOLAR TAURUS T-7300S	5.00 MW	25.0000 PPMV @ 15% O2	SOLONOX BURNER. LOW NOX BURNER	BACT-OTHER
DIGHTON POWER ASSOCIATE, LP	MA	4B96096	10/6/97	TURBINE, COMBUSTION, ABB GT11N2	1327.00 MMBTU/H	17.1200 LB/H	DRY LOW NOX COMBUSTION TECHNOLOGY WITH SCR ADD-ON NOX CONTROL	BACT-PSD
NORTHERN CALIFORNIA POWER AGENCY	CA	N-583-1-1	10/2/97	GE FRAME 5 GAS TURBINE	325.00 MMBTU/HR	25.0000 PPMVD @ 15% O2	DRY LOW NOX BURNERS	LAER
QUESTAR PIPELINE CORP. - RK SPRINGS COMPRESSOR COM	WY	MD-333	9/25/97	TURBINE COMPRESSOR ENGINE, NATURAL GAS FIRED, 2EA	1001.00 HP	2.8000 G/B-HP-H		BACT-PSD
BERKSHIRE POWER DEVELOPMENT, INC	MA	1-X-95-093	9/22/97	ENGINES, CHILLER, NATURAL GAS-FIRED, TWO	23.40 MMBTU/H	0.7000 LB/H	DRY LOW NOX COMBUSTION TECHNOLOGY WITH SCR ADD-ON NOX CONTROL	BACT-PSD
BERKSHIRE POWER DEVELOPMENT, INC	MA	1-X-95-093	9/22/97	TURBINE, COMBUSTION, ABB GT24	1792.00 MMBTU/H	20.3000 LB/H	DRY LOW NOX COMBUSTION TECHNOLOGY WITH SCR ADD-ON NOX CONTROL	BACT-PSD
UNIVERSITY OF MEDICINE & DENTISTRY OF NEW JERSEY	NJ	0874/27/28/29 (3)	6/26/97	COMBUSTION TURBINE COGENERATION UNITS, 3	56.00 MMBTU/H	0.1670 LB/MMBTU NAT.GAS		RACT
LORDSBURG L.P.	NM	PSD-NM-1975	6/18/97	TURBINE, NATURAL GAS-FIRED, ELEC. GEN.	100.00 MW	74.4000 LBS/HR	DRY LOW-NOX TECHNOLOGY WHICH ADOPTS STAGED OR SCHEDULED COMBUSTION	BACT-PSD
SOUTHERN CALIFORNIA GAS COMPANY	CA	S-1792-5-3	5/14/97	VARIABLE LOAD NATURAL GAS FIRED TURBINE COMPRESSOR	50.10 MMBTU/HR	25.0000 PPMVD @ 15% O2	DRY LOW NOX COMBUSTOR	LAER
COLO. POWER PARTNERS- BRUSH COGEN FAC	CO	91MR933	3/27/97	COGEN TURBINES W/ DUCT BURNERS & BOILERS	385.00 MM BTU/HR	42.0000 PPM @ 15% O2	LOW NOX COMBUSTION RETROFIT AND WATER INJECTION	BACT-PSD
MEAD COATED BOARD, INC.	AL	211-0004	3/12/97	COMBINED CYCLE TURBINE (25MW)	568.00 MMBTU/HR	25.0000 PPMVD @ 15% O2 (GAS)	F.O. OIL SULFUR CONTENT <=0.05% BY WT DLN NOX FIRING GAS WITH WATER INJECTION FIRING OIL	BACT-PSD
FORMOSA PLASTICS CORPORATION, BATON ROUGE PLANT	LA	PSD-LA-560 (M-2)	3/7/97	TURBINE/HRSG, GAS COGENERATION	450.00 MM BTU/HR	9.0000 PPMV	DRY LOW NOX BURNER/COMBUSTION DESIGN AND CONSTRUCTION.	BACT-PSD
QUINCY SOYBEAN COMPANY OF ARKANSAS	AR	800A-OP-RO	3/4/97	BOILER, COGENERATION/WASTE HEAT RECOVERY	68.00 MMBTU/H	25.0000 PPM @ 15% O2	LOW NOX COMBUSTORS	BACT-PSD
SOUTHWESTERN PUBLIC SERVICE COMPANY/CUNNINGHAM STA	NM	PSD-NM-622-M-2	2/15/97	COMBUSTION TURBINE, NATURAL GAS	100.00 MW	0.0000 SEE FACILITY NOTES	DRY LOW NOX COMBUSTION	BACT-PSD
CALRESOURCES LLC	CA	S-1543-5-3 AND 6-3	1/10/97	SOLAR MODEL 1100 SATURN GAS TURBINE	13.60 MMBTU/HR	69.0000 PPMVD @ 15% O2	NO CONTROL	LAER
TEMPO PLASTICS	CA	S-995-5-0	12/31/96	GAS TURBINE COGENERATION UNIT	0.00	0.1090 LB/MMBTU	LOW-NOX COMBUSTOR	LAER
SOUTHERN NATURAL GAS COMPANY	MS	1300-00031	12/17/96	TURBINE, NATURAL GAS-FIRED	9160.00 HORSEPOWER	110.0000 PPMV @ 15% O2 DRY	PROPER TURBINE DESIGN AND OPERATION	BACT-PSD
SOUTHWESTERN PUBLIC SERVICE CO/CUNNINGHAM STATION	NM	PSD-NM-622-M-1	11/4/96	COMBUSTION TURBINE, NATURAL GAS	100.00 MW	15.0000 PPM; SEE FAC. NOTES	DRY LOW NOX COMBUSTION	BACT-PSD
ECOLELECTRICA, L.P.	PR	PR-0102	10/1/96	TURBINES, COMBINED-CYCLE COGENERATION	461.00 MW	73.0000 LB/HR	STEAM/WATER INJECTION AND SELECTIVE CATALYTIC REDUCTION (SCR).	BACT-PSD
ECOLELECTRICA, L.P.	PR	PR-0102	10/1/96	TURBINES, COMBINED-CYCLE COGENERATION	461.00 MW	60.0000 LB/HR	STEAM/WATER INJECTION AND SELECTIVE CATALYTIC REDUCTION (SCR).	BACT-PSD
TOYOTA MOTOR CORPORATION SVCS OF N.A.	IN	CP-051-5391-00037	8/9/96	PLANTWIDE COMBUSTION UNITS	1680.00 MMBTU/HR	0.1300 LB/MMBTU	FUEL SPEC. USE OF NATURAL GAS AS FUEL.	BACT-PSD
BLUE MOUNTAIN POWER, LP	PA	09-328-009	7/31/96	COMBUSTION TURBINE WITH HEAT RECOVERY BOILER	153.00 MW	4.0000 PPM @ 15% O2	DRY LNB WITH SCR, WATER INJECTION FOR OIL FIRING. OIL FIRING LIMITS SET TO 84 PPM @ 15% O2	LAER
WESTPLAINS ENERGY	CO	95BP013	6/14/96	SIMPLE CYCLE TURBINE, NATURAL GAS	218.50 MW	15.0000 PPM @ 15% O2 (@ >75%)	DLN NOX. COMMITMENT TO UPGRADE THE DLN TO NEW VERSIONS EMITTING LOWER NOXAS THEY BECOME AVAILABLE.	BACT-PSD
PUBLIC SERVICE OF COLO.-FORT ST VRAIN	CO	94W6609	5/1/96	COMBINED CYCLE TURBINES (2), NATURAL	471.00 MW	15.0000 PPMVD, SMPL CY	DRY LOW NOX COMBUSTION SYSTEMS FOR TURBINES AND DUCT BURNERS	BACT-PSD
CAROLINA POWER & LIGHT	NC	1812	4/11/96	COMBUSTION TURBINE, 4 EACH	1907.60 MMBTU/HR	512.3000 LB/HR	WATER INJECTION; FUEL SPEC. 0.04% N FUEL OIL	BACT-PSD
CAROLINA POWER & LIGHT	NC	1812	4/11/96	COMBUSTION TURBINE, 4 EACH	1907.60 MMBTU/HR	158.0000 LB/HR	WATER INJECTION	BACT-PSD
MID-GEORGIA COGEN.	GA	4911-076-11753	4/3/96	COMBUSTION TURBINE (2), NATURAL GAS	116.00 MW	9.0000 PPMVD	DRY LOW NOX BURNER WITH SCR	BACT-PSD
MID-GEORGIA COGEN.	GA	4911-076-11753	4/3/96	COMBUSTION TURBINE (2), FUEL OIL	116.00 MW	20.0000 PPMVD	WATER INJECTION WITH SCR	BACT-PSD
GEORGIA GULF CORPORATION	LA	PSD-LA-592	3/26/96	GENERATOR, NATURAL GAS FIRED TURBINE	1123.00 MM BTU/HR	25.0000 PPMV-CORR. TO 15% O2	CONTROL NOX USING STEAM INJECTION	BACT-PSD
SEMINOLE HARDBE UNIT 3	FL	PA-89-258A / PSD-FL-214	1/1/96	COMBINED CYCLE COMBUSTION TURBINE	140.00 MW	15.0000 PPM @ 15% O2	DRY LNB	BACT-PSD
MINNESOTA METHANE	AZ	95-0241	11/12/95	ENGINES, COGENERATION (4)	800.00 KW	99.0000 TPY	AIR/FUEL CONTROLLER ADJUSTED TO OBTAIN LOW NOX.	BACT
KEY WEST CITY ELECTRIC SYSTEM	FL	AC44-245399 / PSD-FL-210	9/28/95	TURBINE, EXISTING CT RELOCATION TO A NEW PLANT	23.00 MW	75.0000 PPM @ 15% O2	WATER INJECTION	BACT-PSD
UNION CARBIDE CORPORATION	LA	PSD-LA-590	9/22/95	GENERATOR, GAS TURBINE	1313.00 MM BTU/HR	25.0000 PPMV CORR. TO 15% O2	DRY LOW NOX COMBUSTOR	BACT-PSD
PUEBTO RICO ELECTRIC POWER AUTHORITY (PREPA)	PR	PR-0100	7/31/95	COMBUSTION TURBINES (3), 83 MW SIMPLE-CYCLE EACH	248.00 MW	35.0000 LB/HR AS NO2	STEAM INJECTION PLUS SCR SYSTEM. USE OF NO. 2 F.O. NITROGEN CONTENT NOT TO EXCEED 0.10% BY WEIGHT.	BACT-PSD
HIGGINSVILLE MUNICIPAL POWER FACILITY	MO	0795-0023	7/27/95	ADD OF A DUAL FUEL FIRED TWIN-PAC TURBINE	49.10 MW	42.0000 PPM BY VOL 1 HR AVG	CONTROLS TO REGULATE THE FUEL CONSUMPTION AND THE RATIO OF WATER TO FUEL BEING FIRED IN THE TURBINES	BACT-PSD
HIGGINSVILLE MUNICIPAL POWER FACILITY	MO	0795-0023	7/27/95	ADD OF A DUAL FUEL FIRED TWIN-PAC TURBINE	49.10 MW	75.0000 PPM BY VOL 1 HR AVG	CONTROLS TO REGULATE THE FUEL CONSUMPTION AND THE RATIO OF WATER TO FUEL BEING FIRED IN THE TURBINES	BACT-PSD
BROOKLYN NAVY YARD COGENERATION PARTNERS L.P.	NY	2-6101-00185/00002-9	6/6/95	TURBINE, OIL FIRED	240.00 MW	10.0000 PPM @ 15% O2	SCR	LAER
BROOKLYN NAVY YARD COGENERATION PARTNERS L.P.	NY	2-6101-00185/00002-9	6/6/95	TURBINE, NATURAL GAS FIRED	240.00 MW	3.5000 PPM @ 15% O2	SCR	LAER
PANDA-KATHELEN, L.P.	FL	AC53-251898/PSD-FL-216	6/1/95	COMBINED CYCLE COMBUSTION TURBINE (TOTAL 115MW)	75.00 MW	15.0000 PPM @ 15% O2	DRY LOW NOX BURNER	BACT-PSD
PROCTOR AND GAMBLE PAPER PRODUCTS CO (CHARMIN)	PA	66-0001	5/31/95	TURBINE, NATURAL GAS	580.00 MMBTU/HR	55.0000 PPM @ 15% O2	STEAM INJECTION	RACT
HOFFMAN-LA ROCHE, NUTLEY COGEN FACILITY	NJ	SEE FACILITY NOTES	5/8/95	TURBINE, GM LM500	86.60 MMBTU/H	0.3400 LB/MMBTU		RACT
GAINESVILLE REGIONAL UTILITIES	FL	PSD-FL-212	4/11/95	SIMPLE CYCLE COMBUSTION TURBINE, GAS/NO 2 OIL B-UP	74.00 MW	15.0000 PPM AT 15% OXYGEN	DRY LOW NOX BURNERS	BACT-PSD
GAINESVILLE REGIONAL UTILITIES	FL	PSD-FL-212	4/11/95	OIL FIRED COMBUSTION TURBINE	74.00 MW	42.0000 PPM AT 15% OXYGEN	WATER INJECTION	BACT-PSD
ALGONQUIN GAS TRANSMISSION COMPANY	NJ	LOG# 94-0079	3/31/95	TURBINES COMBUSTION, TWO SOLAR CENTAUR	3.10 MW EACH	0.0000 NOT APPLICABLE	GOOD COMBUSTION PRACTICE	RACT
ALGONQUIN GAS TRANSMISSION COMPANY	NJ	LOG# 94-0079	3/31/95	TURBINES COMBUSTION, TWO SOLAR CENTAUR	3.10 MW EACH	43.3800 LB/H		BACT
FORMOSA PLASTICS CORPORATION, LOUISIANA	LA	PSD-LA-560 (M-1)	3/2/95	TURBINE/HRSG, GAS COGENERATION	450.00 MM BTU/HR	9.0000 PPMV	DRY LOW NOX BURNER/COMBUSTION DESIGN AND CONTROL	LAER
LSP-COTTAGE GROVE, L.P.	MN	16300087-001	3/1/95	COMBUSTION TURBINE/GENERATOR	1970.00 MMBTU/HR	4.5000 PPM @ 15% O2 GAS	SELECTIVE CATALYTIC REDUCTION (SCR)	BACT-PSD
EMPIRE DISTRICT ELECTRIC CO.	MO	0395-015	2/28/95	INST ALL TWO NEW SIMPLE-CYCLE TURBINES	87.77 MW	360.0000 TPY	WATER INJECTION.	BACT-PSD
MARATHON OIL CO. - INDIAN BASIN N.G. PLAN	NM	PSD-NM-295-M-2	1/11/95	TURBINES, NATURAL GAS (2)	5500.00 HP	7.4000 LBS/HR	LEAN-PREMIUM COMBUST	



Table B-2. Summary of Best Available Control Technology (BACT) Determinations for Nitrogen Oxide (NO<sub>x</sub>) Emissions for Combustion Turbines

Facility Name	State	Permit Number	Permit Issue Date	Unit/Process Description	Capacity (size)	NO <sub>x</sub> Emission Limit	Control Method	Basis
SACRAMENTO COGENERATION AUTHORITY P&G	CA	11436	8/19/94	TURBINE, SIMPLE CYCLE LM6000 GAS	421.40 MMBTU/H	5.0000 PPM @ 15% O <sub>2</sub>	SELECTIVE CATALYTIC REDUCTION AND WATER INJECTION	BACT
SACRAMENTO COGENERATION AUTHORITY P&G	CA	11436	8/19/94	TURBINE, GAS, COMBINED CYCLE LM6000	421.40 MMBTU/H	5.0000 PPM @ 15% O <sub>2</sub>	SELECTIVE CATALYTIC REDUCTION AND WATER INJECTION	BACT
SACRAMENTO COGENERATION AUTHORITY P&G	CA	11436	8/19/94	TURBINE, GAS, COMBINED CYCLE LM6000	421.40 MMBTU/H	3.0000 PPM @ 15% O <sub>2</sub>	SELECTIVE CATALYTIC REDUCTION AND WATER INJECTION	BACT
SACRAMENTO POWER AUTHORITY CAMPBELL SOUP	CA	11456	8/19/94	TURBINE, GAS, COMBINED CYCLE, SIEMENS V84.2	1257.00 MMBTU/H	3.0000 PPMVD @ 15% O <sub>2</sub>	SELECTIVE CATALYTIC REDUCTION AND DRY LOW NOX COMBUSTION	BACT
HERMISTON GENERATING CO.	OR	30-0113	7/7/94	TURBINES, NATURAL GAS (2)	1696.00 MMBTU/H	4.5000 PPM @ 15% O <sub>2</sub>	SCR	BACT-PSD
MUDDY RIVER L.P.	NV	A0113	6/10/94	COMBUSTION TURBINE, DIESEL & NATURAL GAS	140.00 MEGAWATT	303.0000 LB/HR	LOW NOX BURNER	BACT-PSD
CSW NEVADA, INC.	NV	A0116	6/10/94	COMBUSTION TURBINE, DIESEL & NATURAL GAS	140.00 MEGAWATT	273.0000 LB/HR	DRY LOW NOX COMBUSTOR	BACT-PSD
PORTLAND GENERAL ELECTRIC CO.	OR	25-0031	5/31/94	TURBINES, NATURAL GAS (2)	1720.00 MMBTU	4.5000 PPM @ 15% O <sub>2</sub>	SCR	BACT-PSD
EMPIRE DISTRICT ELECTRIC CO.	MO	0594-035	5/17/94	INSTALL TWO NEW SIMPLE-CYCLE TURBINES	1345.00 MMBTU/HR	25.0000 PPM BY VOL 1 HR AVG	LOW NOX BURNERS, AND WATER INJECTION	BACT-PSD
EMPIRE DISTRICT ELECTRIC CO.	MO	0594-035	5/17/94	INSTALL TWO NEW SIMPLE-CYCLE TURBINES	1345.00 MMBTU/HR	1135.0000 TPY	LOW NOX BURNERS, AND WATER INJECTION	BACT-PSD
GEORGIA POWER COMPANY, ROBINS TURBINE PROJECT	GA	4911-076-11348	5/13/94	TURBINE, COMBUSTION, NATURAL GAS	80.00 MW	25.0000 PPM	WATER INJECTION, FUEL SPEC: NATURAL GAS	BACT-PSD
WEST CAMPUS COGENERATION COMPANY	TX	23962/PSD-TX-837	5/2/94	GAS TURBINES	75.30 MW (TOTAL POWER)	200.0000 TPY	INTERNAL COMBUSTION CONTROLS	BACT-PSD
FLEETWOOD COGENERATION ASSOCIATES	PA	06-328-001	4/22/94	NG TURBINE (GE LM6000) WITH WASTE HEAT BOILER	360.00 MMBTU/HR	21.0000 LB/HR	SCR WITH LOW NOX COMBUSTORS	BACT-OTHER
FLORIDA POWER CORPORATION POLK COUNTY SITE	FL	PSD-FL-195	2/25/94	TURBINE, NATURAL GAS (2)	1510.00 MMBTU/H	12.0000 PPMVD @ 15% O <sub>2</sub>	DRY LOW NOX COMBUSTOR	BACT-PSD
FLORIDA POWER CORPORATION POLK COUNTY SITE	FL	PSD-FL-195	2/25/94	TURBINE, FUEL OIL (2)	1730.00 MMBTU/H	42.0000 PPMVD @ 15% O <sub>2</sub>	WATER INJECTION	BACT-PSD
INTERNATIONAL PAPER	LA	PSD-LA-93(M-3)	2/24/94	TURBINE/HRSG, GAS COGEN	338.00 MM BTU/HR TURBINE	25.0000 PPMV 15% O <sub>2</sub> TURBINE	DRY LOW NOX COMBUSTOR/COMBUSTION CONTROL	BACT
TECO POLK POWER STATION	FL	PSD-FL-194	2/24/94	TURBINE, SYNGAS (COAL GASIFICATION)	1755.00 MMBTU/H	25.0000 PPMVD @ 15% O <sub>2</sub>	DRY LOW NOX COMBUSTOR	BACT-PSD
TBCO POLK POWER STATION	FL	PSD-FL-194	2/24/94	TURBINE, FUEL OIL	1765.00 MMBTU/H	42.0000 PPMVD @ 15% O <sub>2</sub>	WET INJECTION	BACT-PSD
KAMINE/BESICORP CARTHAGE L.P.	NY	226001 0265 00001	1/18/94	GE FRAME 6 GAS TURBINE	491.00 BTU/HR	42.0000 PPM, 76.6 LB/HR	STEAM INJECTION	BACT
SUNLAW COGEN (FEDERAL COLD STORAGE COGENERATION)	CA	RECLAIM 55711	1/15/94	TURBINE, NATURAL GAS FIRED, COMBINED CYCLE AND COG	28.00 MW	186817.0000 LB/YR	WATER INJECTION AND SCONOX (MOD 2) CATALYST SYSTEM IS INSTALLED AFTER THE HRSG.	BACT-OTHER
ORANGE COGENERATION LP	FL	PSD-FL-206	12/30/93	TURBINE, NATURAL GAS, 2	368.30 MMBTU/H	15.0000 PPM @ 15% O <sub>2</sub>	DRY LOW NOX COMBUSTOR	BACT-PSD
PROJECT ORANGE ASSOCIATES	NY	311500 2015 00001	12/1/93	GE LM-5000 GAS TURBINE	550.00 MMBTU/HR	25.0000 PPM, 47 LB/HR	STEAM INJECTION, FUEL SPEC: NATURAL GAS ONLY	BACT
WILLIAMS FIELD SERVICES CO. - EL CEDRO COMPRESSOR	NM	PSD-NM-340M2	10/29/93	TURBINE, GAS-FIRED	11257.00 HP	42.0000 PPM @ 15% O <sub>2</sub>	SOLONOX COMBUSTOR, DRY LOW NOX TECHNOLOGY	BACT-PSD
CROCKETT COGENERATION - C&H SUGAR	CA	S-201	10/5/93	TURBINE, GAS, GENERAL ELECTRIC MODEL PG7221 (FA)	240.00 MW	5.0000 PPMVD @ 15% O <sub>2</sub>	DRY LOW-NOX COMBUSTORS AND A MITSUBISHI HEAVY INDUSTRIES AMERICAN SELECTIVE CATALYTIC REDUCTION CATALYST.	BACT-OTHER
FLORIDA GAS TRANSMISSION	FL	FL-PSD-202	9/27/93	TURBINE, GAS	131.59 MMBTU/HR	25.0000 PPM @ 15% O <sub>2</sub>	DRY LOW NOX COMBUSTOR	BACT-PSD
PATOWMACK POWER PARTNERS, LIMITED PARTNERSHIP	VA	71975	9/15/93	TURBINE, COMBUSTION, SIEMENS MODEL V84.2, 3	10.20 X10 <sup>9</sup> SCF/YR NAT GAS	131.0000 LB/HR(GAS); 339 OIL	DRY LOW NOX COMBUSTOR; DESIGN, WATER INJECTION	BACT-PSD
FLORIDA GAS TRANSMISSION COMPANY	AL	503-3028-X003	8/5/93	TURBINE, NATURAL GAS	12600.00 BHP	0.5800 GM/HP HR	AIR-TO-FUEL RATIO CONTROL, DRY LOW NOX COMBUSTION	BACT-PSD
CARSON ENERGY GROUP & CENTRAL VALLEY FINANCING AU	CA	11012	7/23/93	TURBINE, GAS, COMBINED CYCLE, GE LM6000	450.00 MMBTU/H	5.0000 PPMVD @ 15% O <sub>2</sub>	SCR AND WATER INJECTION ALSO HAS CARBON ABSORPTION SYSTEM IN DIGESTER TO REMOVE ORGANSILOXANES	BACT
CARSON ENERGY GROUP & CENTRAL VALLEY FINANCING AU	CA	11012	7/23/93	TURBINE, GAS, SIMPLE CYCLE, GE LM6000	450.00 MMBTU/H	5.0000 PPMVD @ 15% O <sub>2</sub>	SELECTIVE CATALYTIC REDUCTION AND WATER INJECTION	BACT
LOCKPORT COGEN FACILITY	NY	292600 0445/00001-00007	7/14/93	(6) GE FRAME 6 TURBINES (EP #S 00001-00006)	423.90 MMBTU/HR	42.0000 PPM	STEAM INJECTION	BACT
ANITEC COGEN PLANT	NY	030200 0451	7/7/93	GE LM5000 COMBINED CYCLE GAS TURBINE EP #00001	451.00 MMBTU/HR	25.0000 PPM, 41 LB/HR	NO CONTROLS	BACT-OTHER
BANK OF AMERICA LOS ANGELES DATA CENTER	CA	A/N 272850	6/24/93	TURBINE, DIESEL & GENERATOR (SEE NOTES)	0.00	163.0000 PPM @ 15% O <sub>2</sub>	FUEL SPEC: LOW NOX DIESEL FUEL (SEE NOTES)	BACT-OTHER
NEWARK BAY COGENERATION PARTNERSHIP, L.P.	NJ	01-92-5221 TO 01-92-5261	6/9/93	TURBINES, COMBUSTION, NATURAL GAS-FIRED (2)	617.00 MMBTU/HR (EACH)	8.3000 PPMVD	SCR	BACT-PSD
NEWARK BAY COGENERATION PARTNERSHIP, L.P.	NJ	01-92-5221 TO 01-92-5261	6/9/93	TURBINES, COMBUSTION, KEROSENE-FIRED (2)	640.00 MMBTU/HR (EACH)	16.0000 PPMVD	SCR	BACT-PSD
TIGER BAY LP	FL	PSD-FL-190	5/17/93	TURBINE, GAS	1614.80 MMBTU/H	15.0000 PPM @ 15% O <sub>2</sub>	DRY LOW NOX COMBUSTOR	BACT-PSD
TIGER BAY LP	FL	PSD-FL-190	5/17/93	TURBINE, OIL	1849.90 MMBTU/H	42.0000 PPM @ 15% O <sub>2</sub>	WATER INJECTION	BACT-PSD
INDECK ENERGY COMPANY	NY	563203 0099	5/12/93	GE FRAME 6 GAS TURBINE EP #00001	491.00 MMBTU/HR	32.0000 PPM	STEAM INJECTION	BACT
PHOENIX POWER PARTNERS	CO	92WB1357	5/11/93	TURBINE (NATURAL GAS)	311.00 MMBTU/HR	22.0000 PPM @ 15% O <sub>2</sub>	DRY LOW NOX COMBUSTION	BACT-OTHER
LILCO SHOREHAM	NY	472200 5378	5/10/93	(3) GE FRAME 7 TURBINES (EP #S 00007-9)	850.00 MMBTU/HR	35.0000 PPM + FBN & HEAT RATE	WATER INJECTION	BACT
TRIGEN MITCHELL FIELD	NY	282089 4163 00004	4/16/93	GE FRAME 6 GAS TURBINE	424.70 MMBTU/HR	60.0000 PPM, 90 LB/HR	STEAM INJECTION	BACT
KISSIMMEE UTILITY AUTHORITY	FL	FL-PSD-182	4/7/93	TURBINE, NATURAL GAS	869.00 MMBTU/H	15.0000 PPM @ 15% O <sub>2</sub>	DRY LOW NOX COMBUSTOR	BACT-PSD
KISSIMMEE UTILITY AUTHORITY	FL	FL-PSD-182	4/7/93	TURBINE, NATURAL GAS	367.00 MMBTU/H	15.0000 PPM @ 15% O <sub>2</sub>	DRY LOW NOX COMBUSTOR	BACT-PSD
KISSIMMEE UTILITY AUTHORITY	FL	FL-PSD-182	4/7/93	TURBINE, FUEL OIL	928.00 MMBTU/H	42.0000 PPM @ 15% O <sub>2</sub>	WATER INJECTION	BACT-PSD
KISSIMMEE UTILITY AUTHORITY	FL	FL-PSD-182	4/7/93	TURBINE, FUEL OIL	371.00 MMBTU/H	42.0000 PPM @ 15% O <sub>2</sub>	WATER INJECTION	BACT-PSD
EAST KENTUCKY POWER COOPERATIVE	KY	C-93-045	3/24/93	TURBINES (5), #2 FUEL OIL AND NAT. GAS FIRED	1492.00 MMBTU/H (EACH)	42.0000 PPM @ 15% O <sub>2</sub> (OIL)	WATER INJECTION	SEE NOTES
INTERNATIONAL PAPER CO. RIVERDALE MILL	AL	104-0003-X026	1/11/93	TURBINE, STATIONARY (GAS-FIRED) WITH DUCT BURNER	40.00 MW	0.0800 LB/MMBTU (GAS)	LOW NOX BURNERS (ON THE DUCT BURNER) STEAM INJECTION INTO THE TURBINE	BACT-PSD
OKLAHOMA MUNICIPAL POWER AUTHORITY	OK	92-016-C (PSD)	12/17/92	TURBINE, COMBUSTION	58.00 MW	65.0000 PPM @ 15% O <sub>2</sub>	COMBUSTION CONTROLS	BACT-OTHER
OKLAHOMA MUNICIPAL POWER AUTHORITY	OK	92-016-C (PSD)	12/17/92	TURBINE, COMBUSTION	58.00 MW	25.0000 PPM @ 15% O <sub>2</sub>	COMBUSTION CONTROLS	BACT-OTHER
AUBURNDALE POWER PARTNERS, LP	FL	PSD-FL-185	12/14/92	TURBINE, GAS	1214.00 MMBTU/H	15.0000 PPMVD @ 15% O <sub>2</sub>	DRY LOW NOX COMBUSTOR	BACT-PSD
AUBURNDALE POWER PARTNERS, LP	FL	PSD-FL-185	12/14/92	TURBINE, OIL	1170.00 MMBTU/H	42.0000 PPMVD @ 15% O <sub>2</sub>	STEAM INJECTION	BACT-PSD
SITHE/INDEPENDENCE POWER PARTNERS	NY	7-3556-00010-00007-9	11/24/92	TURBINES, COMBUSTION (4) (NATURAL GAS) (1012 MW)	2133.00 MMBTU/HR (EACH)	4.5000 PPM	SCR AND DRY LOW NOX	BACT-OTHER
KAMINE/BESICORP BEAVER FALLS COGENERATION FACILITY	NY	6-2320-00018/00001-0	11/9/92	TURBINE, COMBUSTION (NAT. GAS & OIL FUEL) (79MW)	650.00 MMBTU/HR	55.0000 PPM	DRY LOW NOX OR SCR	BACT-OTHER
KAMINE/BESICORP BEAVER FALLS COGENERATION FACILITY	NY	6-2320-00018/00001-0	11/9/92	TURBINE, COMBUSTION (NAT. GAS & OIL FUEL) (79MW)	650.00 MMBTU/HR	9.0000 PPM	DRY LOW NOX OR SCR	BACT-OTHER
KAMINE/BESICORP CORNING L.P.	NY	8-4638-00222/01-0	11/5/92	TURBINE, COMBUSTION (79 MW)	653.00 MMBTU/HR	9.0000 PPM	DRY LOW NOX OR SCR	BACT-OTHER
GRAYS FERRY CO. GENERATION PARTNERSHIP	PA	92181 TO 92184	11/4/92	TURBINE (NATURAL GAS & OIL)	1150.00 MMBTU	9.0000 PPMVD (NAT. GAS)*	DRY LOW NOX BURNER, COMBUSTION CONTROL	BACT-OTHER
GOAL LINE, LP ICEFLOE	CA	911504	11/3/92	TURBINE, COMBUSTION (NATURAL GAS) (424 MW)	386.00 MMBTU/HR	5.0000 PPMVD @ 15% OXYGEN	WATER INJECTION & SCR W/ AUTOMATIC AMMONIA INJECT.	BACT-OTHER
BEAR ISLAND PAPER COMPANY, L.P.	VA	50840	10/30/92	TURBINE, COMBUSTION GAS	474.00 X10 <sup>6</sup> BTU/HR N. GAS	9.0000 PPM	SELECTIVE CATALYTIC REDUCTION (SCR)	BACT-PSD
BEAR ISLAND PAPER COMPANY, L.P.	VA	50840	10/30/92	TURBINE, COMBUSTION GAS	468.00 X10 <sup>6</sup> BTU/HR #2 OIL	15.0000 PPM	SCR	BACT-PSD
BEAR ISLAND PAPER COMPANY, L.P.	VA	50840	10/30/92	TURBINE, COMBUSTION GAS (TOTAL)	0.00	69.7000 TPY	SCR	BACT-PSD
GORDONSVILLE ENERGY L.P.	VA	REGISTRATION # 40808	9/25/92	TURBINE FACILITY, GAS	1331.13 X10 <sup>7</sup> SCF/Y NAT GAS	245.0000 TOTAL TPY	SELECTIVE CATALYTIC REDUCTION (SCR) W/ WATER INJECT	BACT-PSD
GORDONSVILLE ENERGY L.P.	VA	REGISTRATION # 40808	9/25/92	TURBINE FACILITY, GAS	744 X10 <sup>7</sup> GPY FUEL OIL	245.0000 TOTAL TPY	SELECTIVE CATALYTIC REDUCTION (SCR)	BACT-PSD
GORDONSVILLE ENERGY L.P.	VA	REGISTRATION # 40808	9/25/92	TURBINES (2) [EACH WITH A SF]	1.51 X10 <sup>9</sup> BTU/HR N GAS	9.0000 PPMVD/UNIT @ 15% O <sub>2</sub>	SCR WITH WATER INJECTION	BACT-PSD
GORDONSVILLE ENERGY L.P.	VA	REGISTRATION # 40808	9/25/92	TURBINES (2) [EACH WITH A SF]	1.36 X10 <sup>9</sup> BTU/HR #2 OIL	66.0000 LBS/HR/UNIT	WATER INJECTION AND SCR	BACT-PSD
NEVADA POWER COMPANY, HARRY ALLEN PEAKING PLANT	NV	A533	9/18/92	COMBUSTION TURBINE ELECTRIC POWER GENERATION	600.00 MW (6 UNITS 75 EACH)	88.6000 TPY (EACH TURBINE)	LOW NOX COMBUSTOR	BACT-PSD
KAMINE SOUTH GLENS FALLS COGEN CO	NY	414401 0212 00001	9/10/92	GE FRAME 6 GAS TURBINE	498.00 MMBTU/HR	42.0000 PPM, 76.6 LB/HR	WATER INJECTION	BACT
NORTHERN STATES POWER COMPANY	SD	NONE	9/2/92	TURBINE, SIMPLE CYCLE, 4 EACH	129.00 MW	24.0000 PPM @ 15% O <sub>2</sub> GAS	WATER INJECTION FOR GAS & DISTILLATION	BACT-PSD
PASNY/HOLTSVILLE COMBINED CYCLE PLANT	NY	1-4722-00926/00001-9	9/1/92	TURBINE, COMBUSTION GAS (150 MW)	1146.00 MMBTU/HR (GAS)*	42.0000 PPM	WATER INJECTOR	BACT-OTHER
PASNY/HOLTSVILLE COMBINED CYCLE PLANT	NY	1-4722-00926/00001-9	9/1/92	TURBINE, COMBUSTION GAS (150 MW)	1146.00 MMBTU/HR (GAS)*	9.0000 PPM	DRY LOW NOX	BACT-OTHER
PASNY/HOLTSVILLE COMBINED CYCLE PLANT	NY	1-4722-00926/00001-9	9/1/92	GENERATOR, EMERGENCY (NATURAL GAS)	1.50 MMBTU/HR	1.3000 LB/MMBTU	LEAN BURN ENGINE	BACT-OTHER
WEPCU, PARIS SITE	WI	91-RV-043	8/29/92	TURBINES, COMBUSTION (4)	0.00	65.0000 PPM @ 15% O <sub>2</sub>	GOOD COMBUSTION PRACTICES	BACT-PSD
WEPCU, PARIS SITE	WI	91-RV-043	8/29/92	TURBINES, COMBUSTION (4)	0.00	25.0000 PPM @ 15% O <sub>2</sub>	GOOD COMBUSTION PRACTICES	BACT-PSD
FLORIDA POWER CORPORATION	FL	FL-PSD-180	8/17/92	TURBINE, OIL	1029.00 MMBTU/H	42.0000 PPMVD @ 15% O <sub>2</sub>	WET INJECTION	BACT-PSD
FLORIDA POWER CORPORATION	FL	FL-PSD-180	8/17/92	TURBINE, OIL	1866.00 MMBTU/H	42.0000 PPMVD @ 15% O <sub>2</sub>	WET INJECTION	BACT-PSD
NORTHWEST PIPELINE COMPANY	WA	92-4	8/13/92	TURBINE, GAS-FIRED	12100.00 HP	196.0000 PPM @ 15% O <sub>2</sub>	ADVANCED DRY LOW NOX COMBUSTOR (BY 07/01/95)	BACT-PSD
CNG TRANSMISSION	OH	01-3870	8/12/92	TURBINE (NATURAL GAS) (3)	5500.00 HP (EACH)	1.6000 G/HP-HR*	LOW NOX COMBUSTION	BACT-OTHER
SARANAC ENERGY COMPANY	NY	5-0942-00106/00001-9	7/31/92	TURBINES, COMBUSTION (2) (NATURAL GAS)	1123.00 MMBTU/HR (EACH)	9.0000 PPM	SCR	BACT-OTHER
HARTWELL ENERGY LIMITED PARTNERSHIP	GA	4911-073-10941	7/28/92	TURBINE, GAS FIRED (2 EACH)	1817.00 M BTU/HR	25.0000 PPM @ 15% O <sub>2</sub>	MAXIMUM WATER INJECTION	BACT-PSD
HARTWELL ENERGY LIMITED PARTNERSHIP	GA	4911-073-10941	7/28/92	TURBINE, OIL FIRED (2 EACH)	1840.00 M BTU/HR	25.0000 PPMVD, FUEL N AFLOW	MAXIMUM WATER INJECTION	BACT-PSD
MAUI ELECTRIC COMPANY, LTD./MAALAEA GENERATING STA	HI	HI 90-05	7/28/92	TURBINE, COMBINED-CYCLE COMBUSTION	28.00 MW	42.3000 LB/HR	WATER INJECTION	BACT-OTHER
INDECK-YERKES ENERGY SERVICES	NY	146400 0133	6/24/92	GE FRAME 6 GAS TURBINE (EP #00001)	432.20 MMBTU/HR	42.0000 PPM, 74 LB/HR	STEAM INJECTION	BACT
SELKIRK COGENERATION PARTNERS, L.P.	NY	4-0122-00078/00002-9	6/18/92	COMBUSTION TURBINES (2) (252 MW)	1173.00 MMBTU/HR (EACH)	9.0000 PPM GAS	STEAM INJECTION AND SCR	BACT-OTHER
SELKIRK COGENERATION PARTNERS, L.P.	NY	4-0122-00078/00002-9	6/18/92	COMBUSTION TURBINE (79 MW)	1173.00 MMBTU/HR	25.0000 PPM GAS	STEAM INJECTION	BACT-OTHER
TENASKA WASHINGTON PARTNERS, L.P.	WA	91-04	5/29/92	COGENERATION PLANT, COMBINED CYCLE	1.83 MMBTU/HR	7.0000 PPM @ 15% O <sub>2</sub> (GAS)	STAGED LOW NOX DUCT BURNERS, STEAM INJECTION, SELECTIVE CATALYTIC REDUCTION (SCR)	BACT-PSD
NORTHWEST PIPELINE CORPORATION	CO	91LP792(1-2) MOD. #1	5/29/92	TURBINE, SOLAR TAURUS	45.00 MMBTU/HR	95.0000 PPMVD (UNTIL 11/98)	DRY LOW NOX COMBUSTOR (BY 11/01/98)	BACT-PSD
NARRAGANSITT ELECTRIC/NEW ENGLAND POWER CO.	RI	RI-PSD-4	4/13/92	TURBINE, GAS AND DUCT BURNER	1360.00 MMBTU/HR EACH	9.0000 PPM @ 15% O <sub>2</sub> , GAS	SCR	BACT-PSD
KENTUCKY UTILITIES COMPANY	KY	C-92-005	3/10/92	TURBINE, #2 FUEL OIL/NATURAL GAS (8)	1500.00 MM BTU/HR (EACH)	42.0000 PPM @ 15% O <sub>2</sub> , N. GAS	WATER INJECTION	BACT-PSD

Table B-2. Summary of Best Available Control Technology (BACT) Determinations for Nitrogen Oxide (NO<sub>x</sub>) Emissions for Combustion Turbines

Facility Name	State	Permit Number	Permit Issue Date	Unit/Process Description	Capacity (size)	NO <sub>x</sub> Emission Limit	Control Method	Basis
KALAMAZOO POWER LIMITED	MI	1234-90	12/3/91	TURBINE, GAS-FIRED, 2, W/WASTE HEAT BOILERS	1805.90 MMBTU/H	15.0000 PPMV	DRY LOW NOX TURBINES	BACT-PSD
LAKE COGEN LIMITED	FL	PSD-FL-176	11/20/91	TURBINE, GAS, 2 EACH	42.00 MW	25.0000 PPM @ 15% O <sub>2</sub>	COMBUSTION CONTROL	BACT-PSD
LAKE COGEN LIMITED	FL	PSD-FL-176	11/20/91	TURBINE, OIL, 2 EACH	42.00 MW	42.0000 PPM @ 15% O <sub>2</sub>	COMBUSTION CONTROL	BACT-PSD
ORLANDO UTILITIES COMMISSION	FL	PSD-FL-173	11/5/91	TURBINE, GAS, 4 EACH	35.00 MW	42.0000 PPM @ 15% O <sub>2</sub>	WET INJECTION	BACT-PSD
ORLANDO UTILITIES COMMISSION	FL	PSD-FL-173	11/5/91	TURBINE, OIL, 4 EACH	35.00 MW	65.0000 PPM @ 15% O <sub>2</sub>	WET INJECTION	BACT-PSD
SOUTHERN CALIFORNIA GAS	CA	2046009-011	10/29/91	TURBINE, GAS-FIRED	47.64 MMBTU/H	8.0000 PPMVD @ 15% O <sub>2</sub>	HIGH TEMPERATURE SELECTIVE CATALYTIC REDUCTION	BACT-PSD
SOUTHERN CALIFORNIA GAS	CA	2046009-011	10/29/91	TURBINE, GAS FIRED, SOLAR MODEL H	5500.00 HP	8.0000 PPM @ 15% O <sub>2</sub>	HIGH TEMP SELECT. CAT. REDUCTION	BACT-PSD
EL PASO NATURAL GAS	AZ		10/25/91	TURBINE, GAS, SOLAR CENTAUR H	5500.00 HP	84.9000 PPM @ 15% O <sub>2</sub>	LEAN BURN	NSPS
EL PASO NATURAL GAS	AZ		10/25/91	TURBINE, GAS, SOLAR CENTAUR H	5500.00 HP	42.0000 PPM @ 15% O <sub>2</sub>	DRY LOW NOX COMBUSTOR	BACT-PSD
EL PASO NATURAL GAS	AZ		10/25/91	TURBINE, GAS, SOLAR CENTAUR H	5500.00 HP	85.1000 PPM @ 15% O <sub>2</sub>	FUEL SPEC. LEAN FUEL MIX	NSPS
EL PASO NATURAL GAS	AZ		10/25/91	TURBINE, GAS, SOLAR CENTAUR H	5500.00 HP	42.0000 PPM @ 15% O <sub>2</sub>	DRY LOW NOX COMBUSTOR	BACT-PSD
FLORIDA POWER GENERATION	FL	PSD-FL-167	10/18/91	TURBINE, OIL, 6 EACH	92.90 MW	42.0000 PPM @ 15% O <sub>2</sub>	WET INJECTION	BACT-PSD
EL PASO NATURAL GAS	AZ		10/18/91	TURBINE, NAT. GAS TRANSM., GE FRAME 3	12000.00 HP	225.0000 PPM @ 15% O <sub>2</sub>	LEAN BURN	BACT-PSD
EL PASO NATURAL GAS	AZ		10/18/91	TURBINE, NAT. GAS TRANSM., GE FRAME 3	12000.00 HP	42.0000 PPM @ 15% O <sub>2</sub>	DRY LOW NOX COMBUSTOR	BACT-PSD
NUGGET OIL CO.	CA	4131003	10/8/91	GENERATOR, STEAM, GAS FIRED	62.50 MMBTU/H	0.0430 LBM/MBTU	LOW NOX BURNER AND FLUE GAS RECIRCULATION*	BACT-PSD
SEX POWER SYSTEMS, ENCOGEN NW COGENERATION PROJECT	WA	91-02	9/26/91	TURBINES, COMBINED CYCLE COGEN, GE FRAME 6	123.00 MW	7.0000 PPMVD@15%O <sub>2</sub> NG	STEAM INJECTION AND SCR	BACT-PSD
CAROLINA POWER AND LIGHT CO.	SC	0820-0033-CA TO CC	9/23/91	TURBINE, I.C.	80.00 MW	292.0000 LB/H	WATER INJECTION	BACT-PSD
ENRON LOUISIANA ENERGY COMPANY	LA	PSD-LA-569	8/5/91	TURBINE, GAS, 2	39.10 MMBTU/H	40.0000 PPM @ 15% O <sub>2</sub>	H <sub>2</sub> O INJECT 0.67 LB/LB	BACT-PSD
ALGONQUIN GAS TRANSMISSION CO.	RI	1126-1127	7/31/91	TURBINE, GAS, 2	49.00 MMBTU/H	100.0000 PPM @ 15% O <sub>2</sub>	LOW NOX COMBUSTION	BACT-OTHER
CHARLES LARSEN POWER PLANT	FL	PSD-FL-166	7/25/91	TURBINE, GAS, 1 EACH	80.00 MW	25.0000 PPM @ 15% O <sub>2</sub>	WET INJECTION	BACT-PSD
CHARLES LARSEN POWER PLANT	FL	PSD-FL-166	7/25/91	TURBINE, OIL, 1 EACH	80.00 MW	42.0000 PPM @ 15% O <sub>2</sub>	WET INJECTION	BACT-PSD
SUMAS ENERGY INC.	WA		6/25/91	TURBINE, NATURAL GAS	88.00 MW	6.0000 PPM @ 15% O <sub>2</sub>	SCR	BACT-PSD
SAGUARO POWER COMPANY	NV	A393	6/17/91	COMBUSTION TURBINE GENERATOR	34.50 MW	16.9000 PPH (WINTER)	SELECTIVE CATALYTIC REDUCTION (SCR)	BACT-PSD
FLORIDA POWER AND LIGHT	FL	PSD-FL-146	6/5/91	TURBINE, GAS, 4 EACH	400.00 MW	25.0000 PPM @ 15% O <sub>2</sub>	LOW NOX COMBUSTORS	BACT-PSD
FLORIDA POWER AND LIGHT	FL	PSD-FL-146	6/5/91	TURBINE, CG, 4 EACH	400.00 MW	42.0000 PPM @ 15% O <sub>2</sub>	LOW NOX COMBUSTORS	BACT-PSD
FLORIDA POWER AND LIGHT	FL	PSD-FL-146	6/5/91	TURBINE, OIL, 2 EACH	400.00 MW	65.0000 PPM @ 15% O <sub>2</sub>	LOW NOX COMBUSTORS	BACT-PSD
GRANITE ROAD LIMITED	CA	4216001	5/6/91	TURBINE, GAS, ELECTRIC GENERATION	460.90 MMBTU/H*	3.5000 PPMVD @ 15% O <sub>2</sub>	SCR, STEAM INJECTION	BACT-PSD
NORTHERN CONSOLIDATED POWER	PA	25-328-001	5/3/91	TURBINES, GAS, 2	34.60 KW EACH	25.0000 PPM @ 15% O <sub>2</sub>	STEAM INJECTION/+SCR IN 1997	OTHER
LAKEWOOD COGENERATION, L.P.	NJ	SEVERAL; SEE NOTES	4/1/91	TURBINES (NATURAL GAS) (2)	1190.00 MMBTU/HR (EACH)	0.0330 LBM/MBTU	SCR, DRY LOW NOX BURNER	BACT-OTHER
LAKEWOOD COGENERATION, L.P.	NJ	SEVERAL; SEE NOTES	4/1/91	TURBINES (#2 FUEL OIL) (2)	1190.00 MMBTU/HR (EACH)	0.0820 LBM/MBTU	SCR AND WATER INJECTION	BACT-OTHER
CIMARRON CHEMICAL	CO	90WE438	3/25/91	TURBINE #1, GE FRAME 6	33.00 MW	25.0000 PPM @ 15% O <sub>2</sub>	WATER INJECTION	OTHER
CIMARRON CHEMICAL	CO	90WE438	3/25/91	TURBINE #2, GE FRAME 6	33.00 MW	9.0000 PPM @ 15% O <sub>2</sub>	SCR	OTHER
SEMINOLE FERTILIZER CORPORATION	FL	PSD-FL-157	3/17/91	TURBINE, GAS	26.00 MW	9.0000 PPM @ 15% O <sub>2</sub>	SCR	BACT-PSD
FLORIDA POWER AND LIGHT	FL	PSD-FL-145	3/14/91	TURBINE, GAS, 4 EACH	240.00 MW	42.0000 PPM @ 15% O <sub>2</sub>	COMBUSTION CONTROL	BACT-PSD
FLORIDA POWER AND LIGHT	FL	PSD-FL-145	3/14/91	TURBINE, OIL, 4 EACH	0.00	65.0000 PPM @ 15% O <sub>2</sub>	COMBUSTION CONTROL	BACT-PSD
NEVADA COGENERATION ASSOCIATES #2	NV	A391	1/17/91	COMBINED-CYCLE POWER GENERATION	85.00 MW POWER OUTPUT	61.2600 LBS/HR	SELECTIVE CATALYTIC SYSTEM ON ONE UNIT	BACT-PSD
NEVADA COGENERATION ASSOCIATES #1	NV	A360	1/17/91	COMBINED-CYCLE POWER GENERATION	85.00 MW TOTAL OUTPUT	61.2600 LBS/HR	SELECTIVE CATALYTIC SYSTEM ON ONE UNIT	BACT-PSD
NEWARK BAY COGENERATION PARTNERSHIP	NJ		11/1/90	TURBINE, KEROSENE FIRED	585.00 MMBTU/HR	0.0630 LBM/MBTU	STEAM INJECTION AND SCR	BACT-PSD
NEWARK BAY COGENERATION PARTNERSHIP	NJ		11/1/90	TURBINE, NATURAL GAS FIRED	585.00 MMBTU/HR	0.0630 LBM/MBTU	STEAM INJECTION AND SCR	BACT-PSD
TBG COGEN COGENERATION PLANT	NY	282400 5705 00001	8/5/90	GE LM2500 GAS TURBINE	214.90 MMBTU/HR	75.0000 PPM + FBN CORRECTION	WATER INJECTION	BACT
PEPCO - CHALK POINT PLANT	MD		6/25/90	TURBINE, 105 MW OIL FIRED ELECTRIC	105.00 MW	25.0000 PPM @ 15% O <sub>2</sub>	DRY PREMIX BURNER	BACT-PSD
PEPCO - CHALK POINT PLANT	MD		6/25/90	TURBINE, 84 MW OIL FIRED ELECTRIC	84.00 MW	58.0000 PPM @ 15% O <sub>2</sub>	QUIET COMBUSTION AND WATER INJECTION	BACT-PSD
PEPCO - CHALK POINT PLANT	MD		6/25/90	TURBINE, 105 MW NATURAL GAS FIRED ELECTRIC	105.00 MW	77.0000 PPM @ 15% O <sub>2</sub>	DRY PREMIX AND WATER INJECTION	BACT-PSD
PEPCO - CHALK POINT PLANT	MD		6/25/90	TURBINE, 84 MW NATURAL GAS FIRED ELECTRIC	84.00 MW	25.0000 PPM @ 15% O <sub>2</sub>	QUIET COMBUSTION AND WATER INJECTION	BACT-PSD
PACIFIC GAS TRANSMISSION COMPANY	OR	16-0026	6/19/90	TURBINE GAS, COMPRESSOR STATION	110.00 MMBTU/HR	199.0000 PPM @ 15% O <sub>2</sub>	LOW NOX BURNER DESIGN	NSPS
PEPCO - STATION A	MD		5/31/90	TURBINE, 124 MW OIL FIRED	125.00 MW	77.0000 PPM @ 15% O <sub>2</sub>	WATER INJECTION	BACT-PSD
PEPCO - STATION A	MD		5/31/90	TURBINE, 124 MW NATURAL GAS FIRED	125.00 MW	42.0000 PPM @ 15% O <sub>2</sub>	WATER INJECTION	BACT-PSD
PEDRICKTOWN COGENERATION LIMITED PARTNERSHIP	NJ		2/23/90	TURBINE, NATURAL GAS FIRED	1000.00 MMBTU/HR	0.0440 LBM/MBTU	STEAM INJECTION AND SCR	BACT-PSD
SC ELECTRIC AND GAS COMPANY - HAGOOD STATION	SC	0560-0029	12/11/89	INTERNAL COMBUSTION TURBINE	110.00 MEGAWATTS	308.0000 LBS/HR	WATER INJECTION	BACT-PSD
PEABODY MUNICIPAL LIGHT PLANT	MA	MBR-89-COM-032	11/30/89	TURBINE, 38 MW OIL FIRED	412.00 MMBTU/HR	40.0000 PPM @ 15% O <sub>2</sub>	WATER INJECTION	BACT-OTHER
PEABODY MUNICIPAL LIGHT PLANT	MA	MBR-89-COM-032	11/30/89	TURBINE, 38 MW NATURAL GAS FIRED	412.00 MMBTU/HR	25.0000 PPM @ 15% O <sub>2</sub>	WATER INJECTION	BACT-OTHER
PACIFIC GAS TRANSMISSION	OR	16-0026	11/3/89	TURBINE, NAT. GAS	14600.00 HP	42.0000 PPM @ 15% O <sub>2</sub>	LOW NOX BURNERS	BACT-PSD
SOUTHERN MARYLAND ELECTRIC COOPERATIVE (SMECO)	MD		10/1/89	TURBINE, OIL FIRED ELECTRIC	90.00 MW	400.0000 LB/HR	WATER INJECTION	BACT-PSD
SOUTHERN MARYLAND ELECTRIC COOPERATIVE (SMECO)	MD		10/1/89	TURBINE, NATURAL GAS FIRED ELECTRIC	90.00 MW	199.0000 LB/HR	WATER INJECTION	BACT-PSD
KINGSBURG ENERGY SYSTEMS	CA	3040230101	9/28/89	TURBINE, NATURAL GAS FIRED, DUCT BURNER	34.50 MW	6.0000 PPM @ 15% O <sub>2</sub>	SCR, STEAM INJECTION	BACT-PSD
MEGAN-RACINE ASSOCIATES, INC	NY	402201 0295 00001	8/5/89	GE LM5000-N COMBINED CYCLE GAS TURBINE	401.00 LBM/MBTU	42.0000 PPMVD @ 15% O <sub>2</sub>	WATER INJECTION	BACT
UNOCAL	CA	A/N 168294 AND 168295	7/18/89	TURBINE, GAS (SEE NOTES)	0.00	9.0000 PPM @ 15% O <sub>2</sub>	SELECTIVE CATALYTIC REDUCTION (SCR), WATER INJECTN	BACT-OTHER
KERN FRONT LIMITED	CA	S-1120-1-7	11/4/86	TURBINE, GAS, GENERAL ELECTRIC LM-2500	25.00 MW	96.9600 LB/D	WATER INJECTION AND SELECTIVE CATALYTIC REDUCTION	BACT-OTHER
TOYOTA MOTOR MANUFACTURING U.S.A. INC.	KY	C-86-117	7/17/86	COMBUSTION, NATURAL GAS	0.00	0.1000 LBM/MBTU	WATER INJECTION AND SELECTIVE CATALYTIC REDUCTION	BACT-PSD
UNION ELECTRIC CO	MO	0579-014 TO 0579-015	5/6/79	CONSTRUCTION OF A NEW OIL FIRED COMBUSTION TURBINE	622.00 MMBTU/HR	5242.0000 TPY	WATER INJECTION FOR NOX EMISSIONS	BACT-PSD
PILGRIM ENERGY CENTER	NY	472800 2054		(2) WESTINGHOUSE W501D5 TURBINES (EP #S 00001&2)	1400.00 MMBTU/HR	4.5000 PPM, 23.6 LB/HR	STEAM INJECTION FOLLOWED BY SCR	BACT
LEDERLE LABORATORIES	NY	392400 0095		(2) GAS TURBINES (EP #S 00101&102)	110.00 MMBTU/HR	42.0000 PPM, 18 LB/HR	STEAM INJECTION	BACT-PSD
BRUSH COGENERATION PARTNERSHIP	CO	91MR9341		TURBINE	350.00 MMBTU/HR	25.0000 PPM @ 15% O <sub>2</sub>	DRY LOW NOX BURNER	BACT-PSD
COLORADO POWER PARTNERSHIP	CO	91MR9331-2		TURBINES, 2 NAT GAS & 2 DUCT BURNERS	385.00 MMBTU/HR EACH TURBINE	42.0000 PPM @ 15% O <sub>2</sub>	WATER INJECTION	BACT-PSD
MILAGRO, WILLIAMS FIELD SERVICE	NM	PSD-NM-859-M-4		TURBINE/COGEN, NATURAL GAS (2)	900.00 MMCF/DAY	9.0000 PPM @ 15% O <sub>2</sub>	DRY LOW NOX (GENERAL ELECTRIC MODEL PG6541B)	BACT-PSD
BALTIMORE GAS & ELECTRIC - PERRYMAN PLANT	MD			TURBINE, 140 MW OIL FIRED ELECTRIC	140.00 MW	65.0000 PPM @ 15% O <sub>2</sub>	WATER INJECTION	BACT-PSD
BALTIMORE GAS & ELECTRIC - PERRYMAN PLANT	MD			TURBINE, 140 MW NATURAL GAS FIRED ELECTRIC	140.00 MW	15.0000 PPM @ 15% O <sub>2</sub>	DRY BURN LOW NOX BURNERS	BACT-PSD

Source: EPA RBLC Fourth Quarter 1999 Update

Table B-3. Capital Cost for Selective Catalytic Reduction for General Electric Frame 7 Simple Cycle Combustion Turbine

Cost Component	Costs	Basis of Cost Component
<b>Direct Capital Costs</b>		
SCR Associated Equipment	\$2,835,000	Vendor Estimate
Ammonia Storage Tank	\$126,000	\$35 per 1,000 lb mass flow developed from vendor quotes
Flue Gas Ductwork	\$61,370	Vatavauk,1990
Instrumentation	\$50,000	Additional NO <sub>x</sub> Monitor and System
Taxes	\$170,100	6% of SCR Associated Equipment and Catalyst
Freight	\$141,750	5% of SCR Associated Equipment
<b>Total Direct Capital Costs (TDCC)</b>	<b>\$3,384,220</b>	
<b>Direct Installation Costs</b>		
Foundation and supports	\$270,738	8% of TDCC ; OAQPS Cost Control Manual
Handling & Erection	\$473,791	14% of TDCC ; OAQPS Cost Control Manual
Electrical	\$135,369	4% of TDCC ; OAQPS Cost Control Manual
Piping	\$67,684	2% of TDCC ; OAQPS Cost Control Manual
Insulation for ductwork	\$33,842	1% of TDCC ; OAQPS Cost Control Manual
Painting	\$33,842	1% of TDCC ; OAQPS Cost Control Manual
Site Preparation	\$5,000	Engineering Estimate
Buildings	\$15,000	Engineering Estimate
<b>Total Direct Installation Costs (TDIC)</b>	<b>\$1,035,266</b>	
<b>Total Capital Costs (TCC)</b>	<b>\$4,419,486</b>	Sum of TDCC, TDIC and RCC
<b>Indirect Costs</b>		
Engineering	\$338,422	10% of TDCC; OAQPS Cost Control Manual
PSM/RMP Plan	\$50,000	Engineering Estimate
Construction and Field Expense	\$169,211	5% of TDCC; OAQPS Cost Control Manual
Contractor Fees	\$338,422	10% of TDCC; OAQPS Cost Control Manual
Start-up	\$67,684	2% of TDCC; OAQPS Cost Control Manual
Performance Tests	\$33,842	1% of TDCC; OAQPS Cost Control Manual
Contingencies	\$101,527	3% of TDCC; OAQPS Cost Control Manual
<b>Total Indirect Capital Cost (TInCC)</b>	<b>\$1,099,108</b>	
<b>Total Direct, Indirect and Capital Costs (TDICC)</b>	<b>\$5,518,594</b>	Sum of TCC and TInCC
Mass Flow of Combustion Turbine	3,600,000 lb/hr	"F"

Table B-4. Annualized Cost for Selective Catalytic Reduction for General Electric Frame 7 Simple Cycle Operation

Cost Component	Costs	Basis of Cost Component
<u>Direct Annual Costs</u>		
Operating Personnel	\$18,720	24 hours/week at \$15/hr
Supervision	\$2,808	15% of Operating Personnel; OAQPS Cost Control Manual
Ammonia	\$60,856	\$300 per ton for Aqueous NH <sub>3</sub>
PSM/RMP Update	\$15,000	Engineering Estimate
Inventory Cost	\$40,663	Capital Recovery (10.98%) for 1/3 catalyst
Catalyst Cost	\$370,333	3 years catalyst life; Based on Vendor Budget Estimate
Contingency	\$15,251	3% of Direct Annual Costs
<b>Total Direct Annual Costs (TDAC)</b>	<b>\$523,631</b>	
<u>Energy Costs</u>		
Electrical	\$10,848	80kW/h for SCR @ \$0.04/kWh times Capacity Factor
MW Loss and Heat Rate Penalty	\$162,069	0.3% of MW output; EPA, 1993 (Page 6-20); 2" w.g. pressure drop
<b>Total Energy Costs (TEC)</b>	<b>\$172,917</b>	
<u>Indirect Annual Costs</u>		
Overhead	\$49,430	60% of Operating/Supervision Labor and Ammonia
Property Taxes	\$55,186	1% of Total Capital Costs
Insurance	\$55,186	1% of Total Capital Costs
Annualized Total Direct Capital	\$605,942	10.98% Capital Recovery Factor of 7% over 15 years times sum of TDICC
<b>Total Indirect Annual Costs (TIAC)</b>	<b>\$765,744</b>	
<b>Total Annualized Costs</b>	<b>\$1,462,292</b>	Sum of TDAC, TEC and TIAC
<b>Cost Effectiveness</b>	<b>\$10,466</b>	NO <sub>x</sub> Reduction Only
	<b>\$19,760</b>	Net Emission Reduction

Table B-5. Comparison of Alternative BACT Control Technologies for NO<sub>x</sub> on the Simple-cycle Unit

	Alternative BACT Control Technologies	
	DLN/WI Only	DLN/WI with SCR
Technical Assessment	Feasible	Feasible for gas
Economic Impact <sup>a</sup>		
Capital Costs	included	\$5,518,594
Annualized Costs	included	\$1,462,292
Cost Effectiveness		
NO <sub>x</sub> Removed (per ton of NO <sub>x</sub> )	NA	\$10,466
NO <sub>x</sub> Removed (per ton of total pollutants)	NA	\$19,760
Environmental Impact <sup>b</sup>		
Total NO <sub>x</sub> (TPY)	215	75.2
NO <sub>x</sub> Reduction (TPY)	NA	(139.8)
Ammonia Emissions (TPY)	0	42.6
PM Emissions (TPY)	0	20.8
Secondary Emissions (TPY)	0	2.3
Net Emission Reduction (TPY)	NA	(74.1)
Energy Impacts <sup>c</sup>		
Energy Use (kWh/yr)	0	2,044,848
Energy Use (mmBtu/yr) at 10,000 Btu/kWh	0	19,804
Energy Use (mmcf/yr) at 1,000 Btu/cf for natural gas	0	20

<sup>a</sup> See Tables B-3 and B-4 for detailed development of capital costs (including recurring costs) and annualized costs.

<sup>b</sup> See emission data presented in Table B-6.

<sup>c</sup> Energy impacts are estimated due to the lost energy from heat rate penalty and electrical usage for the SCR operation at 3,390 hours per year. Lost energy is based on 0.3 percent of 174.4 MW. SCR electrical usage is based on 0.080 MWh per SCR system.

Table B-6. Maximum Potential Incremental Emissions (TPY) with Selective Catalytic Reduction  
Simple Cycle Operation

Pollutants	Incremental Emissions (tons/year) of SCR		Total
	Primary	Secondary	
Particulate	20.83	0.07	20.90
Sulfur Dioxide		0.03	0.03
Nitrogen Oxides	-139.72	1.32	-138.40
Carbon Monoxide		0.79	0.79
Volatile Organic Compounds		0.05	0.05
Ammonia	42.62		
	Total:	2.26	-74.00
Carbon Dioxide (additional from gas firing)		1,254.28	1,254.28

Basis:

Lost Energy (mmBtu/year)

19,804

Secondary Emissions (lb/mmBtu): Assumes natural gas firing in NO<sub>x</sub> controlled steam unit.

Particulate

0.0072

Sulfur Dioxide

0.0027

Nitrogen Oxides w/LNB

0.1333

Carbon Monoxide

0.0800

Volatile Organic Compounds

0.0052

Reference: Table 1.4-1 and 1.4-2, AP-42, Version 2/98

Table B-7. Summary of Best Available Control Technology (BACT) Determinations for CO Emissions for Combustion Turbines

Facility Name	State	Permit Number	Permit Issue Date	Unit/Process Description	Capacity (size)	CO Emission Limit	Control Method	Basis
KISSIMMEE UTILITIES AUTHORITY	FL	PSD-FL-254	12/16/99	TURBINE, COMBUSTION	250.00 MW	12.0000 PPM	GOOD COMBUSTION	BACT-PSD
DUKE ENERGY NEW SOMYRNA BEACH POWER CO. LP	FL	PSD-FL-257	10/15/99	TURBINE-GAS, COMBINED CYCLE	500.00 MW (2 UNITS)	12.0000 PPM	GOOD COMBUSTION	BACT-PSD
OLEANDER POWER PROJECT	FL	PSD-FL-258	10/1/99	TURBINE-GAS, COMBINED CYCLE	190.00 MW	12.0000 PPM @ 15% O2	GOOD COMBUSTION	BACT-PSD
PDC EL PASO MILFORD LLC	CT	105-0068	4/16/99	TURBINE, COMBUSTION, ABB GT-24, #1 WITH 2 CHILLE	1.97 MMCF/H	13.0000 LB/H NAT GAS	OXIDATION CATALYST	BACT-PSD
PDC EL PASO MILFORD LLC	CT	105-0069	4/16/99	TURBINE, COMBUSTION, ABB GT-24E, #2 WITH 2 CHILL	1.97 MMCF/H	13.0000 LB/H NAT GAS	OXIDATION CATALYST	BACT-PSD
ALABAMA POWER COMPANY - THEODORE COGENERATION	AL	503-8073	3/16/99	TURBINE, WITH DUCT BURNER	170.00 MW	0.0860 LB/MMBTU	EFFICIENT COMBUSTION	BACT-PSD
WYANDOTTE ENERGY	MI	279-98	2/8/99	TURBINE, COMBINED CYCLE, POWER PLANT	500.00 MW	3.0000 PPM	CATALYTIC OXIDIZER	LAER
MOBILE ENERGY LLC	AL	503-8066	1/5/99	TURBINE, GAS, COMBINED CYCLE	168.00 MW	0.0400 LB/MMBTU	GOOD COMBUSTION PRACTICES	BACT-PSD
TENUSKA GEORGIA PARTNERS, L.P.	GA	4-11-149-0004-P-01-0	12/18/98	TURBINE, COMBUSTION, SIMPLE CYCLE, 6	160.00 MW EA	15.0000 PPMVD @ 15% O2	USING 15% EXCESS AIR. CO EMISSION IS BECAUSE OF NATURAL GAS.	BACT-PSD
TENUSKA GEORGIA PARTNERS, L.P.	GA	4-11-149-0004-P-01-0	12/18/98	TURBINE, COMBUSTION, SIMPLE CYCLE, 6	160.00 MW EA	33.0000 PPMVD	CO EMISSION IS BECAUSE OF FUEL OIL. WHEN OUTPUT IS BELOW 123 MW LIMIT IS 33 PPMVD AND ABOVE 123 MW	BACT-PSD
WESTBROOK POWER LLC	ME	A-743-71-A-N	12/4/98	TURBINE, COMBINED CYCLE, TWO	528.00 MW TOTAL	15.0000 PPM @ 15% O2	USING 15 % EXCESS AIR.	BACT-PSD
GORHAM ENERGY LIMITED PARTNERSHIP	ME	A-735	12/4/98	TURBINE, COMBINED CYCLE	900.00 MW TOTAL	5.0000 PPM @ 15% O2 (NAT G)	0.05% SULFUR DISTILLATE OIL #2 IS USED. EMISSION IS FROM EACH 300 MW SYSTEM.	BACT-PSD
SANTA ROSA ENERGY LLC	FL	PSD-FL 253	12/4/98	TURBINE, COMBUSTION, NATURAL GAS	241.00 MW	0.0000	DRY LOW NOX BURNER	GOOD COMBUSTION PRACTICE
CHAMPION INTERNATL CORP. & CHAMP. CLEAN ENERGY	ME	A-22-71-N-A	9/14/98	TURBINE, COMBINED CYCLE, NATURAL GAS	175.00 MW	9.0000 PPMVD @ 15% O2 GAS		BACT-OTHE
ALABAMA POWER PLANT BARRY	AL	503-1001	8/7/98	TURBINES, COMBUSTION, NATURAL GAS	510.00 MW(TOTAL)	0.0570 LB/MMBTU	EFFICIENT COMBUSTION	BACT-PSD
TNP TECHN, LLC (FORMERLY TX-NM POWER CO.)	NM	PSD-NM-90-M2	8/7/98	GAS TURBINES	375.00 MMBTU/H	18.0000 PPM	GOOD COMBUSTION PRACTICES	BACT-PSD
CASCO RAY ENERGY CO	ME	A-728	7/13/98	TURBINE, COMBINED CYCLE, NATURAL GAS, TWO	170.00 MW EACH	20.0000 PPM @ 15% O2	15% EXCESS AIR	BACT-PSD
CITY OF LAKELAND ELECTRIC AND WATER UTILITIES	FL	PSD-FL-245	7/10/98	TURBINE, COMBUSTION, GAS FIRED W/ FUEL OIL ALSO	2174.00 MMBTU/H	25.0000 PPM	GOOD COMBUSTION WITH DRY LOW NOX BURNERS	OXIDATION CATALYST MAY BE USED
COLORADO SPRINGS UTILITIES-NIXON POWER PLANT	CO	94EP132	6/30/98	SIMPLE CYCLE TURBINE, NATURAL GAS	1122.00 MM BTU/HR	0.8000 DRE	CATALYTIC OXIDATION	BACT-PSD
BRIDGEPORT ENERGY, LLC	CT	0150190 & 0150191	6/29/98	TURBINES, COMBUSTION MODEL V84.3A, 2 SIEMES	260.00 MW/HRSG PER TURBINE	10.0000 PPM GAS & OIL	PRE-MIX FUEL FAIR TO OPTIMIZE EFFICIENCY ACTUAL EMISSIONS EXPECTED BETWEEN 5-7PPM	BACT-PSD
ENCOGEN HAWAII, L.P.	HI	0243-01-C	6/8/98	TURBINES, COMBUSTION, 2 EA	23.00 MW	57.5000 PPMVD @ 15% O2	GOOD COMBUSTION DESIGN AND OPERATION.	BACT-PSD
CITY OF TALLAHASSEE UTILITY SERVICES	FL	PSD-FL-239	5/29/98	TURBINE, COMBINED CYCLE, MULTIPLE FUELS	1468.00 MMBTU/H	0.0000 SEE P2 DESCRIPTION	GOOD COMBUSTION OF CLEAN FUELS	BACT-OTHE
GENERAL ELECTRIC PLASTICS	AL	207-0008-X016	5/27/98	COMBINED CYCLE (TURBINE AND DUCT BURNER)	0.00	0.0800 LBS/MMBTU	PROPER COMBUSTION	BACT-PSD
RUMFORD POWER ASSOCIATES	ME	A-724-71-A-N	5/1/98	TURBINE GENERATOR, COMBUSTION, NATURAL GAS	1906.00 MMBTU/H	15.0000 PPM @ 15% O2	GE DRY LOW-NOX COMBUSTOR DESIGN. GOOD COMBUSTION CONTROL.	BACT-PSD
ANDROSCOGGIN ENERGY LIMITED	ME	A-718-71-A-N	3/31/98	GAS TURBINES, COGEN, W/DUCT BURNERS	675.00 MMBTU/H TURBINE	74.2100 LB/H NG	CATALYTIC OXIDATION, GOOD COMBUSTION PRACTICES.	BACT-PSD
ANDROSCOGGIN ENERGY LIMITED	ME	A-718-71-A-N	3/31/98	GAS TURBINES, COGEN, W/DUCT BURNERS	675.00 MMBTU/H TURBINE	43.7300 LB/H NG OIL	CATALYTIC OXIDATION, GOOD COMBUSTION PRACTICES.	BACT-PSD
TWO ELK GENERATION PARTNERS, LIMITED PARTNERSHIP	WY	CT-1352	2/27/98	TURBINE, STATIONARY	33.30 MW	25.0000 PPM @ 15% O2		OTHER
TIVERTON POWER ASSOCIATES	RI	RI-PSD-5	2/13/98	COMBUSTION TURBINE, NATURAL GAS	265.00 MW	12.0000 PPM @ 15% O2	GOOD COMBUSTION	BACT-PSD
AIR LIQUIDE AMERICA CORPORATION	LA	PSD-LA-622	2/13/98	TURBINE GAS, GE, 7ME 7	966.00 MMBTU/H	25.0000 PPMV	GOOD EQUIPMENT DESIGN, PROPER COMBUSTION TECHNIQUE AND MIN. 2% EXCESS O2	BACT-PSD
MILLENNIUM POWER PARTNER, LP	MA	130921	2/2/98	TURBINE, COMBUSTION, WESTINGHOUSE MODEL 501	2534.00 MMBTU/H	0.0700 LB/MMBTU	DRY LOW NOX COMBUSTION TECHNOLOGY IN CONJUNCTION WITH SCR ADD-ON NOX CONTROL.	BACT-PSD
MAUI ELECTRIC COMPANY	HI	0067-01-C	1/6/98	TURBINE, COMBUSTION, 2 EA	20.00 MW	44.0000 PPMVD @ 15% O2	GOOD COMBUSTION DESIGN AND OPERATION.	BACT-PSD
BASF CORPORATION	LA	PSD-LA-613	12/30/97	DUCT BURNER, COGEN UNIT NO. 2	0.40 MMLB/H STEAM	83.9300 LB/HR	GOOD DESIGN, PROPER OPERATING PRACTICES, 2% EXCESS O2	BACT-PSD
BASF CORPORATION	LA	PSD-LA-613	12/30/97	TURBINE, COGEN UNIT 2, GE FRAME 6	42.40 MW	83.9300 LB/MMBTU	GOOD DESIGN, PROPER COMBUSTION TECHNIQUES, 2% EXCESS O2	BACT-PSD
BUCKNELL UNIVERSITY	PA	60-0001A	11/26/97	NG FIRED TURBINE, SOLAR TAURUS T-7300S	5.00 MW	50.0000 PPMV @ 15% O2	GOOD COMBUSTION	BACT-OTHE
DIGHTON POWER ASSOCIATE, LP	MA	4B96096	10/6/97	TURBINE, COMBUSTION, ABB GT11N2	1327.00 MMBTU/H	5.9700 LB/H	DRY LOW NOX COMBUSTION TECHNOLOGY WITH SCR ADD-ON NOX CONTROL.	BACT-PSD
BERKSHIRE POWER DEVELOPMENT, INC.	MA	1-X-95-093	9/22/97	TURBINE, COMBUSTION, ABB GT24	1792.00 MMBTU/H	14.3000 LB/H	DRY LOW NOX COMBUSTION TECHNOLOGY WITH SCR ADD-ON NOX CONTROL.	BACT-PSD
UNIVERSITY OF MEDICINE & DENTISTRY OF NEW JERSEY	NJ	087427/28/29 (3)	6/26/97	COMBUSTION TURBINE COGENERATION UNITS, 3	56.00 MMBTU/H	75.0000 PPMVD NAT. GAS		RACT
LORDSBURG L.P.	NM	PSD-NM-1975	6/18/97	TURBINE, NATURAL GAS-FIRED, ELEC. GEN.	100.00 MW	27.0000 LBS/HR	DRY LOW-NOX TECHNOLOGY BY MAINTAINING PROPER AIR- FUEL RATIO.	BACT-PSD
COLO. POWER PARTNERS- BRUSH COGEN FAC	CO	91MR933	3/27/97	COGEN TURBINES W/ DUCT BURNERS & BOILERS	385.00 MM BTU/HR	35.0000 PPM @ 15% O2	GOOD COMBUSTION	BACT-PSD
MEAD COATED BOARD, INC.	AL	211-0004	3/12/97	COMBINED CYCLE TURBINE (25 MW)	568.00 MMBTU/HR	28.0000 PPMVD @ 15% O2 (GAS)	PROPER DESIGN AND GOOD COMBUSTION PRACTICES	BACT-PSD
FORMOSA PLASTICS CORPORATION, BATON ROUGE PLANT	LA	PSD-LA-560 (M-2)	3/7/97	TURBINE/HRSG, GAS COGENERATION	450.00 MM BTU/HR	70.0000 LB/HR	COMBUSTION DESIGN AND CONSTRUCTION.	BACT-PSD
SOUTHWESTERN PUBLIC SERVICE COMPANY/CUNNINGHAM STA	NM	PSD-NM-622-M-2	2/15/97	COMBUSTION TURBINE, NATURAL GAS	100.00 MW	0.0000 SEE FACILITY NOTES	GOOD COMBUSTION PRACTICES	BACT-PSD
ECO ELECTRICA, L.P.	PR	PR-0102	10/1/96	TURBINES, COMBINED-CYCLE COGENERATION	461.00 MW	100.0000 PPMVD AT MIN. LOAD	COMBUSTION CONTROLS.	BACT-PSD
ECO ELECTRICA, L.P.	PR	PR-0102	10/1/96	TURBINES, COMBINED-CYCLE COGENERATION	461.00 MW	33.0000 PPMVD	COMBUSTION CONTROLS.	BACT-PSD
BLUE MOUNTAIN POWER, LP	PA	09-328-009	7/31/96	COMBUSTION TURBINE WITH HEAT RECOVERY BOILE	153.00 MW	3.1000 PPM @ 15% O2	OXIDATION CATALYST	16 PPM @ 15% O2 WHEN FIRING NO. 2 OIL. AT 75% NG LIMIT SET TO 22.1 PP
COMMONWEALTH CHESAPEAKE CORPORATION	VA	40898	5/21/96	3 COMBUSTION TURBINES (OIL-FIRED)	6000.00 HRS/YR	96.0000 TPY	GOOD COMBUSTION OPERATING PRACTICES	BACT/NSPS
PORTSIDE ENERGY CORP.	IN	CP 127 5260	5/13/96	TURBINE, NATURAL GAS-FIRED	63.00 MEGAWATT	40.0000 LBS/HR	GOOD COMBUSTION AND EMISSIONS NOT TO EXCEED 40 PPMVD AT 15% OXYGEN.	BACT-PSD
PORTSIDE ENERGY CORP.	IN	CP 127 5260	5/13/96	TURBINE, NATURAL GAS-FIRED	63.00 MEGAWATT	12.0000 LBS/HR	GOOD COMBUSTION AND EMISSIONS NOT TO EXCEED 10 PPMVD AT 15% OXYGEN.	BACT-PSD
PUBLIC SERVICE OF COLO.-FORT ST VRAIN	CO	94WE609	5/1/96	COMBINED CYCLE TURBINES (2), NATURAL	471.00 MW	15.0000 PPMVD, SMPL CY	GOOD COMBUSTION CONTROL PRACTICES. COMMITMENT TO A PATTERN OF OPERATION (LOAD VARIATIONS, ET	BACT-PSD
GENERAL ELECTRIC GAS TURBINES	SC	1200-0094	4/19/96	I.C. TURBINE	2700.00 MMBTU/HR	27169.0000 LB/HR	GOOD COMBUSTION PRACTICES TO MINIMIZE EMISSIONS	BACT-PSD
CAROLINA POWER & LIGHT	NC	1812	4/11/96	COMBUSTION TURBINE, 4 EACH	1907.60 MMBTU/HR	81.0000 LB/HR	COMBUSTION CONTROL	BACT-PSD
CAROLINA POWER & LIGHT	NC	1812	4/11/96	COMBUSTION TURBINE, 4 EACH	1907.60 MMBTU/HR	80.0000 LB/HR	COMBUSTION CONTROL	BACT-PSD
SOUTH MISSISSIPPI ELECTRIC POWER ASSOC.	MS	1360-00035	4/9/96	COMBUSTION TURBINE, COMBINED CYCLE	1299.00 MMBTU/HR NAT GAS	26.3000 PPM @ 15% O2, GAS	GOOD COMBUSTION CONTROLS	BACT-PSD
MID-GEORGIA COGEN.	GA	4911-076-11753	4/3/96	COMBUSTION TURBINE (2), NATURAL GAS	116.00 MW	10.0000 PPMVD	COMPLETE COMBUSTION	BACT-PSD
MID-GEORGIA COGEN.	GA	4911-076-11753	4/3/96	COMBUSTION TURBINE (2), FUEL OIL	116.00 MW	30.0000 PPMVD	COMPLETE COMBUSTION	BACT-PSD
GEORGIA GULF CORPORATION	LA	PSD-LA-592	3/26/96	GENERATOR, NATURAL GAS FIRED TURBINE	1123.00 MM BTU/HR	972.4000 TPY CAP FOR 3 TURB.	GOOD COMBUSTION PRACTICE AND PROPER OPERATION	BACT-PSD
SEMINOLE HARDEE UNIT 3	FL	PA-89-258A / PSD-FL-214	1/1/96	COMBINED CYCLE COMBUSTION TURBINE	140.00 MW	20.0000 PPM (NAT. GAS)	DRY LNB	GOOD COMBUSTION PRACTICES
MINNESOTA METHANE	AZ	95-0241	11/12/95	ENGINES, COGENERATION (4)	800.00 KW	99.9000 TPY	AIR/FUEL CONTROLLER	BACT
KEY WEST CITY ELECTRIC SYSTEM	FL	AC44-245399 / PSD-FL-210	9/28/95	TURBINE, EXISTING CT RELOCATION TO A NEW PLAN	23.00 MW	20.0000 PPM @ 15% O2 FULL LD	GOOD COMBUSTION	BACT-PSD
UNION CARBIDE CORPORATION	LA	PSD-LA-590	9/22/95	DUCT BURNER	710.00 MM BTU/HR	198.6000 LB/HR COMMON VENT	NO ADD-ON CONTROL	GOOD COMBUSTION PRACTICE
UNION CARBIDE CORPORATION	LA	PSD-LA-590	9/22/95	GENERATOR, GAS TURBINE	1313.00 MM BTU/HR	198.6000 LB/HR	NO ADD-ON CONTROL	GOOD COMBUSTION PRACTICE
PUERTO RICO ELECTRIC POWER AUTHORITY (PREPA)	PR	PR-0100	7/31/95	COMBUSTION TURBINES (3), 83 MW SIMPLE-CYCLE EA	248.00 MW	104.0000 LB/HR	MAINTAIN EACH TURBINE IN GOOD WORKING ORDER AND IMPLEMENT GOOD COMBUSTION PRACTICES.	BACT-PSD
PUERTO RICO ELECTRIC POWER AUTHORITY (PREPA)	PR	PR-0100	7/31/95	COMBUSTION TURBINES (3), 83 MW SIMPLE-CYCLE EA	248.00 MW	20.0000 LB/HR	MAINTAIN EACH TURBINE IN GOOD WORKING ORDER AND IMPLEMENT GOOD COMBUSTION PRACTICES.	BACT-PSD
BROOKLYN NAVY YARD COGENERATION PARTNERS L.P.	NY	2-6101-00185/00002-9	6/6/95	TURBINE, OIL FIRED	240.00 MW	5.0000 PPM @ 15% O2		LAER
BROOKLYN NAVY YARD COGENERATION PARTNERS L.P.	NY	2-6101-00185/00002-9	6/6/95	GENERATOR, 3000 KW EMERGENCY	3000.00 KW	0.2500 LB/MMBTU		LAER
BROOKLYN NAVY YARD COGENERATION PARTNERS L.P.	NY	2-6101-00185/00002-9	6/6/95	TURBINE, NATURAL GAS FIRED	240.00 MW	4.0000 PPM @ 15% O2		LAER
PANDA-KATHLEEN, L.P.	FL	AC53-251898/PSD-FL-216	6/1/95	COMBINED CYCLE COMBUSTION TURBINE (TOTAL 115	75.00 MW	25.0000 PPM @ 15% O2	COMBUSTION CONTROLS	STANDARD ONLY APPLIES IF GE CT IS SELECTED, THE ABB CT WAS LESS
ALGONQUIN GAS TRANSMISSION COMPANY	NJ	LOG # 94-0079	3/31/95	TURBINES COMBUSTION, TWO SOLAR CENTAUR	3.10 MW EACH	15.2000 LB/H		BACT
FORMOSA PLASTICS CORPORATION, LOUISIANA	LA	PSD-LA-560 (M-1)	3/2/95	TURBINE/HRSG, GAS COGENERATION	450.00 MM BTU/HR	25.8000 LB/HR	PROPER OPERATION	BACT-PSD
EMPIRE DISTRICT ELECTRIC CO.	MO	0395-015	2/28/95	INSTALL TWO NEW SIMPLE-CYCLE TURBINES	88.77 MW	427.5000 TPY	GOOD COMBUSTION CONTROL	BACT-PSD
MARATHON OIL CO. - INDIAN BASIN N.G. PLAN	NM	PSD-NM-295-M-2	1/11/95	TURBINES, NATURAL GAS (2)	5500.00 HP	13.2000 LBS/HR	LEAN-PREMIUM COMBUSTION TECHNOLOGY.	BACT-PSD
KAMINE/BESICORP SYRACUSE LP	NY	313201 2010/00001-00007	12/10/94	SIEMENS V64.3 GAS TURBINE (EP #00001)	650.00 MMBTU/HR	9.5000 PPM	NO CONTROLS	BACT-OTHE
INDECK-OSWEGO ENERGY CENTER	NY	351200 0211 00001	10/6/94	DUCT BURNER	30.00 MMBTU/HR	0.1280 LB/MMBTU, 3.84 LB/HR	NO CONTROLS	BACT-OTHE
INDECK-OSWEGO ENERGY CENTER	NY	351200 0211 00001	10/6/94	GE FRAME 6 GAS TURBINE	533.00 LB/MMBTU	10.0000 PPM, 10.00 LB/HR	NO CONTROLS	BACT-OTHE
FULTON COGEN PLANT	NY	350400 0221 00001	9/15/94	GE LMS000 GAS TURBINE	500.00 MMBTU/HR	107.0000 PPM, 120 LB/HR	NO CONTROLS	BACT-OTHE
CAROLINA POWER AND LIGHT	SC	0820-0033	8/31/94	STATIONARY GAS TURBINE	1520.00 MMBTU/H	414.0000 LB/H	PROPER OPERATION TO ACHIEVE GOOD COMBUSTION	BACT-PSD
CAROLINA POWER AND LIGHT	SC	0820-0033	8/31/94	STATIONARY GAS TURBINE	1520.00 MMBTU/H	702.0000 LB/H	PROPER OPERATION TO ACHIEVE GOOD COMBUSTION	BACT-PSD
BEAR MOUNTAIN LIMITED	CA	S-2049-1-2	8/19/94	TURBINE, GE, COGENERATION, 48 MW	48.00 MW	252.6000 LB/D	OXIDATION CATALYST	BACT-OTHE
HERMISTON GENERATING CO.	OR	30-0113	7/7/94	TURBINES, NATURAL GAS (2)	1696.00 MMBTU/H	15.0000 PPM @ 15% O2	GOOD COMBUSTION PRACTICES	BACT-PSD
MUDDY RIVER L.P.	NV	A0113	6/10/94	COMBUSTION TURBINE, DIESEL & NATURAL GAS	140.00 MEGAWATT	77.0000 LB/HR	FUEL SPEC: NATURAL GAS	BACT-PSD
CSW NEVADA, INC.	NV	A0116	6/10/94	COMBUSTION TURBINE, DIESEL & NATURAL GAS	140.00 MEGAWATT	83.0000 LB/HR	FUEL SPEC: NATURAL GAS	BACT-PSD
PORTLAND GENERAL ELECTRIC CO.	OR	25-0031	5/31/94	TURBINES, NATURAL GAS (2)	1720.00 MMBTU	15.0000 PPM @ 15% O2	GOOD COMBUSTION PRACTICES	BACT-PSD
EMPIRE DISTRICT ELECTRIC CO.	MO	0594-035	5/17/94	INSTALL TWO NEW SIMPLE-CYCLE TURBINES	345.00 MMBTU/HR	120.0000 TPY	NONE	BACT-PSD
EMPIRE DISTRICT ELECTRIC CO.	MO	0594-035	5/17/94	INSTALL TWO NEW SIMPLE-CYCLE TURBINES	1345.00 MMBTU/HR	1290.0000 TPY	NONE	BACT-PSD



Table B-7. Summary of Best Available Control Technology (BACT) Determinations for CO Emissions for Combustion Turbines

Facility Name	State	Permit Number	Permit Issue Date	Unit/Process Description	Capacity (size)	CO Emission Limit	Control Method	Basis
WEST CAMPUS COGENERATION COMPANY	TX	23962/PSD-TX-837	5/2/94	GAS TURBINES	75.30 MW (TOTAL POWER)	300.0000 TPY	INTERNAL COMBUSTION CONTROLS	BACT
FLORIDA POWER CORPORATION POLK COUNTY SITE	FL	PSD-FL-195	2/25/94	TURBINE, NATURAL GAS (2)	1510.00 MMBTU/H	25.0000 PPMVD	GOOD COMBUSTION PRACTICES	BACT-PSD
FLORIDA POWER CORPORATION POLK COUNTY SITE	FL	PSD-FL-195	2/25/94	TURBINE, FUEL OIL (2)	1730.00 MMBTU/H	30.0000 PPMVD	GOOD COMBUSTION PRACTICES	BACT-PSD
INTERNATIONAL PAPER	LA	PSD-LA-93(M-3)	2/24/94	TURBINE/HRSG, GAS COGEN	338.00 MM BTU/HR TURBINE	165.9000 LB/HR	COMBUSTION CONTROL	BACT
TECO POLK POWER STATION	FL	PSD-FL-194	2/24/94	TURBINE, SYNGAS (COAL GASIFICATION)	1755.00 MMBTU/H	25.0000 PPMVD	GOOD COMBUSTION	BACT-PSD
TECO POLK POWER STATION	FL	PSD-FL-194	2/24/94	TURBINE, FUEL OIL	1765.00 MMBTU/H	40.0000 PPMVD	GOOD COMBUSTION	BACT-PSD
KAMINE/BESICORP CARTHAGE L.P.	NY	226001 0285 00001	1/18/94	GE FRAME 6 GAS TURBINE	491.00 BTU/HR	10.0000 PPM, 11.0 LB/HR	NO CONTROLS	BACT-OTHE
ORANGE COGENERATION LP	FL	PSD-FL-206	12/30/93	TURBINE, NATURAL GAS, 2	368.30 MMBTU/H	30.0000 PPMVD	GOOD COMBUSTION	BACT-PSD
PROJECT ORANGE ASSOCIATES	NY	311500 2015 00001	12/1/93	STACK (TURBINE AND DUCT BURNER)	715.00 MMBTU/HR	106.4000 LB/HR TEMP > 20F	OXIDATION CATALYST	BACT
PROJECT ORANGE ASSOCIATES	NY	311500 2015 00001	12/1/93	GE LM-5000 GAS TURBINE	550.00 MMBTU/HR	92.0000 LB/HR TEMP > 20F	NO CONTROLS	BACT-OTHE
WILLIAMS FIELD SERVICES CO. - EL CEDRO COMPRESSOR	NM	PSD-NM-340M2	10/29/93	TURBINE, GAS-FIRED	11257.00 HP	50.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
CROCKETT COGENERATION - C&H SUGAR	CA	S-201	10/5/93	TURBINE, GAS, GENERAL ELECTRIC MODEL PG7221(FA)	240.00 MW	5.9000 PPMVD @ 15% O2	ENGELHARD OXIDATION CATALYST	BACT-OTHE
PATOWMACK POWER PARTNERS, LIMITED PARTNERSHIP	VA	71975	9/15/93	TURBINE, COMBUSTION, SIEMENS MODEL V84.2, 3	10.20 X109 SCF/YR NAT GAS	26.0000 LB/HR	GOOD COMBUSTION OPERATING PRACTICES	BACT-PSD
FLORIDA GAS TRANSMISSION COMPANY	AL	503-3028-X003	8/5/93	TURBINE, NATURAL GAS	12600.00 BHP	0.4200 GM/HP HR	AIR-TO-FUEL RATIO CONTROL, DRY COMBUSTION CONTROLS	BACT-PSD
LOCKPORT COGEN FACILITY	NY	292600 0446/00001-00007	7/14/93	(3) DUCT BURNER (EP #S 00001-00003)	94.10 MMBTU/HR	0.1000 LB/MMBTU, 9.4 LB/HR	NO CONTROLS	BACT-OTHE
LOCKPORT COGEN FACILITY	NY	292600 0446/00001-00007	7/14/93	(6) GE FRAME 6 TURBINES (EP #S 00001-00006)	423.90 MMBTU/HR	10.0000 PPM	NO CONTROLS	BACT-OTHE
ANITEC COGEN PLANT	NY	030200 0451	7/7/93	DUCT BURNER EP #00001	70.00 MMBTU/HR	0.0350 LB/MMBTU, 2.5 LB/HR	NO CONTROLS	BACT-OTHE
ANITEC COGEN PLANT	NY	030200 0451	7/7/93	GE LM5000 COMBINED CYCLE GAS TURBINE EP #00001	451.00 MMBTU/HR	36.0000 PPM, 33 LB/HR	BAFFLE CHAMBER	SEE NOTE #
NEWARK BAY COGENERATION PARTNERSHIP, L.P.	NJ	01-92-5231 TO 01-92-5261	6/9/93	TURBINES, COMBUSTION, NATURAL GAS-FIRED (2)	617.00 MMBTU/HR (EACH)	1.8000 PPMVD	OXIDATION CATALYST	OTHER
NEWARK BAY COGENERATION PARTNERSHIP, L.P.	NJ	01-92-5231 TO 01-92-5261	6/9/93	TURBINES, COMBUSTION, KEROSENE-FIRED (2)	640.00 MMBTU/HR (EACH)	2.6000 PPMVD	OXIDATION CATALYST	OTHER
PSI ENERGY, INC. WABASH RIVER STATION	IN	CP 167 2610	5/27/93	COMBINED CYCLE SYNGAS TURBINE	1775.00 MMBTU/HR	15.0000 LESS THAN PPM	OPERATION PRACTICES AND GOOD COMBUSTION, COMBINED CYCLE SYNGAS TURBINE	BACT-PSD
TIGER BAY LP	FL	PSD-FL-190	5/17/93	DUCT BURNER, GAS	100.00 MMBTU/H	10.0000 LB/H	GOOD COMBUSTION PRACTICES	BACT-PSD
TIGER BAY LP	FL	PSD-FL-190	5/17/93	TURBINE, GAS	1614.80 MMBTU/H	49.0000 LB/H	GOOD COMBUSTION PRACTICES	BACT-PSD
TIGER BAY LP	FL	PSD-FL-190	5/17/93	TURBINE, OIL	1849.90 MMBTU/H	98.4000 LB/H	GOOD COMBUSTION PRACTICES	BACT-PSD
INDECK ENERGY COMPANY	NY	563203 0099	5/12/93	DUCT BURNER EP #00001	100.00 MMBTU/HR	0.1400 LB/MMBTU, 12.0 LB/HR	NO CONTROLS	BACT-OTHE
INDECK ENERGY COMPANY	NY	563203 0099	5/12/93	GE FRAME 6 GAS TURBINE EP #00001	491.00 MMBTU/HR	40.0000 PPM	NO CONTROLS	BACT-OTHE
PHOENIX POWER PARTNERS	CO	92WEL357	5/11/93	GENERATOR, STEAM, W/ DUCT BURNER	50.00 MMBTU/HR	91.1800 TPY	FUEL SPEC: NATURAL GAS COMBUSTION	OTHER
LILCO SHOREHAM	NY	472200 5378	5/10/93	(3) GE FRAME 7 TURBINES (EP #S 00007-9)	850.00 MMBTU/HR	10.0000 PPM, 19.7 LB/HR	NO CONTROLS	BACT-OTHE
TRIGEN MITCHEL FIELD	NY	282089 4163 00004	4/16/93	GE FRAME 6 GAS TURBINE	424.70 MMBTU/HR	10.0000 PPM, 10.0 LB/HR	NO CONTROLS	BACT-OTHE
KISSIMMEE UTILITY AUTHORITY	FL	FL-PSD-182	4/7/93	TURBINE, NATURAL GAS	869.00 MMBTU/H	54.0000 LB/H	GOOD COMBUSTION PRACTICES	BACT-PSD
KISSIMMEE UTILITY AUTHORITY	FL	FL-PSD-182	4/7/93	TURBINE, NATURAL GAS	367.00 MMBTU/H	40.0000 LB/H	GOOD COMBUSTION PRACTICES	BACT-PSD
KISSIMMEE UTILITY AUTHORITY	FL	FL-PSD-182	4/7/93	TURBINE, FUEL OIL	928.00 MMBTU/H	65.0000 LB/H	GOOD COMBUSTION PRACTICES	BACT-PSD
KISSIMMEE UTILITY AUTHORITY	FL	FL-PSD-182	4/7/93	TURBINE, FUEL OIL	371.00 MMBTU/H	76.0000 LB/H	GOOD COMBUSTION PRACTICES	BACT-PSD
EAST KENTUCKY POWER COOPERATIVE	KY	C-93-045	3/24/93	TURBINES (5), #2 FUEL OIL AND NAT. GAS FIRED	1492.00 MMBTU/HR (EACH)	75.0000 LBS/H (EACH)	PROPER COMBUSTION TECHNIQUES	BACT-OTHE
INTERNATIONAL PAPER CO. RIVERDALE MILL	AL	104-0003-X026	1/11/93	TURBINE, STATIONARY (GAS-FIRED) WITH DUCT BURN	40.00 MW	22.1000 LB/HR	DESIGN	BACT-PSD
AUBURNDALE POWER PARTNERS, LP	FL	PSD-FL-185	12/14/92	TURBINE, GAS	1214.00 MMBTU/H	15.0000 PPMVD	GOOD COMBUSTION PRACTICES	BACT-PSD
AUBURNDALE POWER PARTNERS, LP	FL	PSD-FL-185	12/14/92	TURBINE, OIL	1170.00 MMBTU/H	25.0000 PPMVD	GOOD COMBUSTION PRACTICES	BACT-PSD
SITHE/INDEPENDENCE POWER PARTNERS	NY	7-3556-00040-00007-9	11/24/92	TURBINES, COMBUSTION (4) (NATURAL GAS) (1012 MW)	2133.00 MMBTU/HR (EACH)	13.0000 PPM	COMBUSTION CONTROLS	BACT-OTHE
KAMINE/BESICORP BEAVER FALLS COGENERATION FACILITY	NY	6-2320-00018/00001-0	11/9/92	TURBINE, COMBUSTION (NAT. GAS & OIL FUEL) (79MW)	650.00 MMBTU/HR	9.5000 PPM	COMBUSTION CONTROLS	BACT-OTHE
GRAYS FERRY CO. GENERATION PARTNERSHIP	PA	92181 TO 92184	11/4/92	TURBINE (NATURAL GAS & OIL)	1150.00 MMBTU	0.0055 LB/MMBTU (GAS)*	COMBUSTION	BACT-OTHE
GRAYS FERRY CO. GENERATION PARTNERSHIP	PA	92181 TO 92184	11/4/92	GENERATOR, STEAM	450.00 MMBTU	0.0055 LB/MMBTU (NAT GAS)*	COMBUSTION	BACT-OTHE
BEAR ISLAND PAPER COMPANY, L.P.	VA	50840	10/30/92	TURBINE, COMBUSTION GAS	474.00 X10(6) BTU/HR N. GAS	11.0000 LBS/HR	GOOD COMBUSTION	BACT-PSD
BEAR ISLAND PAPER COMPANY, L.P.	VA	50840	10/30/92	TURBINE, COMBUSTION GAS	468.00 X10(6) BTU/HR #2 OIL	11.0000 LBS/HR	GOOD COMBUSTION	BACT-PSD
BEAR ISLAND PAPER COMPANY, L.P.	VA	50840	10/30/92	TURBINE, COMBUSTION GAS (TOTAL)	0.00	48.2000 TPY	GOOD COMBUSTION	BACT-PSD
GORDONVILLE ENERGY L.P.	VA	REGISTRATION # 40808	9/25/92	TURBINE FACILITY, GAS	1331.13 X10(7) SCF/Y NAT GAS	249.9000 TOTAL TPY	GOOD COMBUSTION PRACTICES	BACT-PSD
GORDONVILLE ENERGY L.P.	VA	REGISTRATION # 40808	9/25/92	TURBINE FACILITY, GAS	7.44 X10(7) GPY FUEL OIL	249.9000 TOTAL TPY	GOOD COMBUSTION PRACTICES	BACT-PSD
GORDONVILLE ENERGY L.P.	VA	REGISTRATION # 40808	9/25/92	TURBINES (2) [EACH WITH A SF]	1.51 X10(9) BTU/HR N GAS	57.0000 LBS/HR/UNIT	GOOD COMBUSTION PRACTICES	BACT-PSD
GORDONVILLE ENERGY L.P.	VA	REGISTRATION # 40808	9/25/92	TURBINES (2) [EACH WITH A SF]	1.36 X10(9) BTU/HR #2 OIL	68.0000 LBS/HR/UNIT	GOOD COMBUSTION PRACTICES	BACT-PSD
NEVADA POWER COMPANY, HARRY ALLEN PEAKING PLANT	NV	A533	9/18/92	COMBUSTION TURBINE ELECTRIC POWER GENERATI	600.00 MW (8 UNITS 75 EACH)	152.5000 TPY (EACH TURBINE)	PRECISION CONTROL FOR THE LOW NOX COMBUSTOR	BACT-PSD
KAMINE SOUTH GLENS FALLS COGEN CO	NY	414401 0212 00001	9/10/92	GE FRAME 6 GAS TURBINE	498.00 MMBTU/HR	9.0000 PPM, 11.0 LB/HR	NO CONTROLS	BACT-OTHE
NORTHERN STATES POWER COMPANY	SD	NONE	9/2/92	TURBINE, SIMPLE CYCLE, 4 EACH	129.00 MW	50.0000 PPM FOR GAS	GOOD COMBUSTION TECHNIQUES	BACT-PSD
PASNY/HOLTSVILLE COMBINED CYCLE PLANT	NY	1-4722-00926/00001-9	9/1/92	GENERATOR, EMERGENCY (NATURAL GAS)	1.50 MMBTU/HR	6.5000 LB/MMBTU	COMBUSTION CONTROL	BACT-OTHE
PASNY/HOLTSVILLE COMBINED CYCLE PLANT	NY	1-4722-00926/00001-9	9/1/92	TURBINE, COMBUSTION GAS (150 MW)	1146.00 MMBTU/HR (GAS)*	8.5000 PPM	COMBUSTION CONTROL	BACT-OTHE
WPCU, PARIS SITE	WI	91-RV-043	8/29/92	TURBINES, COMBUSTION (4)	0.00	25.0000 LBS/HR (SEE NOTES)	COMBUSTION CONTROL	BACT-PSD
FLORIDA POWER CORPORATION	FL	FL-PSD-180	8/17/92	TURBINE, OIL	1029.00 MMBTU/H	54.0000 LB/H	GOOD COMBUSTION PRACTICES	BACT-PSD
FLORIDA POWER CORPORATION	FL	FL-PSD-180	8/17/92	TURBINE, OIL	1866.00 MMBTU/H	79.0000 LB/H	GOOD COMBUSTION PRACTICES	BACT-PSD
CNG TRANSMISSION	OH	01-3870	8/12/92	TURBINE (NATURAL GAS) (3)	5500.00 HP (EACH)	0.0150 G/HP-HR	FUEL SPEC: USE OF NATURAL GAS	OTHER
SARANAC ENERGY COMPANY	NY	5-0942-00106/00001-9	7/31/92	BURNERS, DUCT (2)	553.00 MMBTU/HR EACH	0.0600 LB/MMBTU	OXIDATION CATALYST	BACT-OTHE
SARANAC ENERGY COMPANY	NY	5-0942-00106/00001-9	7/31/92	TURBINES, COMBUSTION (2) (NATURAL GAS)	1123.00 MMBTU/HR (EACH)	3.0000 PPM	OXIDATION CATALYST	BACT-OTHE
HARTWELL ENERGY LIMITED PARTNERSHIP	GA	4911-073-10941	7/28/92	TURBINE, GAS FIRED (2 EACH)	1817.00 M BTU/HR	25.0000 PPMVD @ FULL LOAD	FUEL SPEC: CLEAN BURNING FUELS	BACT-PSD
HARTWELL ENERGY LIMITED PARTNERSHIP	GA	4911-073-10941	7/28/92	TURBINE, OIL FIRED (2 EACH)	1840.00 M BTU/HR	25.0000 PPMVD @ FULL LOAD	FUEL SPEC: CLEAN BURNING FUELS	BACT-PSD
MAUI ELECTRIC COMPANY, LTD./MAALAEA GENERATING STA	HI	HI 90-05	7/28/92	TURBINE, COMBINED-CYCLE COMBUSTION	28.00 MW	26.9000 LB/HR	COMBUSTION TECHNOLOGY/DESIGN	BACT-OTHE
INDECK-YERKES ENERGY SERVICES	NY	146400 0133	6/24/92	DUCT BURNER (EP #00001)	20.00 MMBTU/HR	0.0400 LB/MMBTU, 0.8 LB/HR	NO CONTROLS	BACT-OTHE
INDECK-YERKES ENERGY SERVICES	NY	146400 0133	6/24/92	GE FRAME 6 GAS TURBINE (EP #00001)	432.20 MMBTU/HR	10.0000 PPM, 10 LB/HR	NO CONTROLS	BACT-OTHE
SELKIRK COGENERATION PARTNERS, L.P.	NY	4-0122-00078/00002-9	6/18/92	DUCT BURNERS (2)	206.00 MMBTU/HR (EACH)	0.0730 LB/MMBTU GAS, 100%	COMBUSTION CONTROLS	BACT-OTHE
SELKIRK COGENERATION PARTNERS, L.P.	NY	4-0122-00078/00002-9	6/18/92	DUCT BURNER	123.00 MMBTU/HR	0.0720 LB/MMBTU GAS (100%)	COMBUSTION CONTROL	BACT-OTHE
SELKIRK COGENERATION PARTNERS, L.P.	NY	4-0122-00078/00002-9	6/18/92	COMBUSTION TURBINES (2) (252 MW)	1173.00 MMBTU/HR (EACH)	10.0000 PPM	COMBUSTION CONTROLS	BACT-OTHE
SELKIRK COGENERATION PARTNERS, L.P.	NY	4-0122-00078/00002-9	6/18/92	COMBUSTION TURBINE (79 MW)	1173.00 MMBTU/HR	25.0000 PPM	COMBUSTION CONTROL	BACT-OTHE
TENASKA WASHINGTON PARTNERS, L.P.	WA	91-04	5/29/92	COGENERATION PLANT, COMBINED CYCLE	1.83 MMBTU/HR	20.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
NORTHWEST PIPELINE CORPORATION	CO	91LP792(1-2) MOD. #1	5/29/92	BURNERS, DUCT, COEN	29.00 MMBTU/HR PER BURNER	4.0000 LB/HR	OTHER	BACT-PSD
NARRAGANSETT ELECTRIC/NEW ENGLAND POWER CO.	RI	RI-PSD-4	4/13/92	TURBINE, GAS AND DUCT BURNER	1360.00 MMBTU/HR EACH	11.0000 PPM @ 15% O2, GAS	COMBUSTION DESIGN	BACT-PSD
KENTUCKY UTILITIES COMPANY	KY	C-92-005	3/10/92	TURBINE, #2 FUEL OIL/NATURAL GAS (8)	1500.00 MM BTU/HR (EACH)	75.0000 LB/HR (EACH)	COMBUSTION CONTROL	BACT-PSD
BERMUDA HUNDRED ENERGY LIMITED PARTNERSHIP	VA	51020	3/3/92	TURBINE, COMBUSTION	1175.00 MMBTU/HR NAT. GAS	62.0000 LB/H/UNIT	FURNACE DESIGN	BACT-PSD
BERMUDA HUNDRED ENERGY LIMITED PARTNERSHIP	VA	51020	3/3/92	TURBINE, COMBUSTION	1117.00 MMBTU/HR NO2 FUEL OIL	62.0000 LB/H/UNIT	FURNACE DESIGN	BACT-PSD
BERMUDA HUNDRED ENERGY LIMITED PARTNERSHIP	VA	51020	3/3/92	TURBINE, COMBUSTION, 2	0.00	229.3000 T/YR/UNIT	COMBUSTION CONTROL	BACT-PSD
THERMO INDUSTRIES, LTD.	CO	9/WEE667(1-5)	2/19/92	TURBINE, GAS FIRED, 5 EACH	246.00 MMBTU/HR	25.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
SAVANNAH ELECTRIC AND POWER CO.	GA	4911-051-8529	2/12/92	TURBINES, 8	1032.00 MMBTU/HR, NAT GAS	9.0000 PPM @ 15% O2	FUEL SPEC: LOW SULFUR FUEL OIL	BACT-PSD
SAVANNAH ELECTRIC AND POWER CO.	GA	4911-051-8529	2/12/92	TURBINES, 8	972.00 MMBTU/HR, #2 OIL	9.0000 PPM @ 15% O2	FUEL SPEC: LOW SULFUR FUEL OIL	BACT-PSD
HAWAII ELECTRIC LIGHT CO., INC.	HI	HI-90-04	2/12/92	TURBINE, FUEL OIL #2	20.00 MW	26.8000 LB/HR @ 100% PEAKLD	COMBUSTION DESIGN	BACT-PSD
HAWAII ELECTRIC LIGHT CO., INC.	HI	HI-90-04	2/12/92	TURBINE, FUEL OIL #2	20.00 MW	56.4000 LB/H @ 75-<100% PKLD	COMBUSTION DESIGN	BACT-PSD
HAWAII ELECTRIC LIGHT CO., INC.	HI	HI-90-04	2/12/92	TURBINE, FUEL OIL #2	20.00 MW	181.0000 LB/H @ 50-<75% PKLD	COMBUSTION DESIGN	BACT-PSD
HAWAII ELECTRIC LIGHT CO., INC.	HI	HI-90-04	2/12/92	TURBINE, FUEL OIL #2	20.00 MW	475.6000 LB/H @ 25-<50% PKLD	COMBUSTION DESIGN	BACT-PSD
KAMINE/BESICORP NATURAL DAM LP	NY	404089 0305 00001	12/31/91	GE FRAME 6 GAS TURBINE	500.00 MMBTU/HR	0.0200 LB/MMBTU, 10 LB/HR	NO CONTROLS	BACT-OTHE
DUKE POWER CO. LINCOLN COMBUSTION TURBINE STATION	NC	7171	12/20/91	TURBINE, COMBUSTION	1313.00 MM BTU/HR	59.0000 LB/HR	COMBUSTION CONTROL	BACT-PSD



Table B-7. Summary of Best Available Control Technology (BACT) Determinations for CO Emissions for Combustion Turbines

Facility Name	State	Permit Number	Permit Issue Date	Unit/Process Description	Capacity (size)	CO Emission Limit	Control Method	Basis
DUKE POWER CO. LINCOLN COMBUSTION TURBINE STATION	NC	7171	12/20/91	TURBINE, COMBUSTION	1247.00 MM BTU/HR	60.0000 LB/HR	COMBUSTION CONTROL	BACT-PSD
MAUI ELECTRIC COMPANY, LTD.	HI	HI-90-02	12/3/91	TURBINE, FUEL OIL #2	28.00 MW	0.0000 SEE NOTES	GOOD COMBUSTION PRACTICES	BACT-PSD
KALAMAZOO POWER LIMITED	MI	1234-90	12/3/91	TURBINE, GAS-FIRED, 2, W/ WASTE HEAT BOILERS	1805.90 MMBTU/H	20.0000 PPMV	DRY LOW NOX TURBINES	BACT-PSD
LAKE COGEN LIMITED	FL	PSD-FL-176	11/20/91	DUCT BURNER, GAS	150.00 MMBTU/H	0.2000 LB/MMBTU	NOT REQUIRED	BACT-PSD
LAKE COGEN LIMITED	FL	PSD-FL-176	11/20/91	TURBINE, GAS, 2 EACH	42.00 MW	42.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
LAKE COGEN LIMITED	FL	PSD-FL-176	11/20/91	TURBINE, OIL, 2 EACH	42.00 MW	78.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
ORLANDO UTILITIES COMMISSION	FL	PSD-FL-173	11/5/91	TURBINE, GAS, 4 EACH	35.00 MW	10.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
ORLANDO UTILITIES COMMISSION	FL	PSD-FL-173	11/5/91	TURBINE, OIL, 4 EACH	35.00 MW	10.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
SOUTHERN CALIFORNIA GAS	CA	2046009-011	10/29/91	TURBINE, GAS-FIRED	47.64 MMBTU/H	7.7400 PPM @ 15% O2	HIGH TEMPERATURE OXIDATION CATALYST	BACT-PSD
SOUTHERN CALIFORNIA GAS	CA	2046009-011	10/29/91	TURBINE, GAS FIRED, SOLAR MODEL H	5500.00 HP	7.7400 PPM @ 15% O2	HIGH TEMP OXIDATION CATALYST	BACT-PSD
EL PASO NATURAL GAS	AZ		10/25/91	TURBINE, GAS, SOLAR CENTAUR H	5500.00 HP	10.5000 PPM @ 15% O2	FUEL SPEC: LEAN FUEL MIX	BACT-PSD
EL PASO NATURAL GAS	AZ		10/25/91	TURBINE, GAS, SOLAR CENTAUR H	5500.00 HP	10.5000 PPM @ 15% O2	FUEL SPEC: LEAN FUEL MIX	BACT-PSD
FLORIDA POWER GENERATION	FL	PSD-FL-167	10/18/91	TURBINE, OIL, 6 EACH	92.90 MW	54.0000 LB/H	COMBUSTION CONTROL	BACT-PSD
EL PASO NATURAL GAS	AZ		10/18/91	TURBINE, NAT. GAS TRANSP., GE FRAME 3	12000.00 HP	60.0000 PPM @ 15% O2	LEAN BURN	BACT-PSD
EEX POWER SYSTEMS, ENCOGEN NW COGENERATION PROJECT	WA	91-02	9/26/91	TURBINES, COMBINED CYCLE COGEN, GE FRAME 6	123.00 MW	10.0000 PPM DV @ 15% O2		BACT-PSD
CAROLINA POWER AND LIGHT CO.	SC	0820-0033-CA TO CC	9/23/91	TURBINE, I.C.	80.00 MW	60.0000 LB/H		BACT-PSD
ENRON LOUISIANA ENERGY COMPANY	LA	PSD-LA-569	8/5/91	TURBINE, GAS, 2	39.10 MMBTU/H	60.0000 PPM @ 15% O2	BASE CASE, NO ADDITIONAL CONTROLS	BACT-PSD
ALGONQUIN GAS TRANSMISSION CO.	RI	1126-1127	7/31/91	TURBINE, GAS, 2	49.00 MMBTU/H	0.1140 LB/MMBTU	GOOD COMBUSTION PRACTICES	BACT-OTHE
CHARLES LARSEN POWER PLANT	FL	PSD-FL-166	7/25/91	TURBINE, GAS, 1 EACH	80.00 MW	25.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
CHARLES LARSEN POWER PLANT	FL	PSD-FL-166	7/25/91	TURBINE, OIL, 1 EACH	80.00 MW	25.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
SUMAS ENERGY INC.	WA		6/25/91	TURBINE, NATURAL GAS	88.00 MW	6.0000 PPM @ 15% O2	CO CATALYST	BACT-PSD
SAGUARO POWER COMPANY	NV	A393	6/17/91	COMBUSTION TURBINE GENERATOR	34.50 MW	9.0000 PPH	CONVERTER (CATALYTIC)	BACT-PSD
FLORIDA POWER AND LIGHT	FL	PSD-FL-146	6/5/91	TURBINE, GAS, 4 EACH	400.00 MW	30.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
FLORIDA POWER AND LIGHT	FL	PSD-FL-146	6/5/91	TURBINE, CG, 4 EACH	400.00 MW	33.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
FLORIDA POWER AND LIGHT	FL	PSD-FL-146	6/5/91	TURBINE, OIL, 2 EACH	400.00 MW	33.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
NORTHERN CONSOLIDATED POWER	PA	25-328-001	5/3/91	TURBINES, GAS, 2	34.60 KW EACH	110.0000 T/YR	OXIDATION CATALYST	OTHER
LAKEWOOD COGENERATION, L.P.	NJ	SEVERAL; SEE NOTES	4/1/91	TURBINES (NATURAL GAS) (2)	1190.00 MMBTU/HR (EACH)	0.0260 LB/MMBTU	TURBINE DESIGN	BACT-OTHE
LAKEWOOD COGENERATION, L.P.	NJ	SEVERAL; SEE NOTES	4/1/91	TURBINES (#2 FUEL OIL) (2)	1190.00 MMBTU/HR (EACH)	0.0600 LB/MMBTU	TURBINE DESIGN	BACT-OTHE
CIMARRON CHEMICAL	CO	90WE438	3/25/91	TURBINE #2, GE FRAME 6	33.00 MW	250.0000 T/YR, LESS THAN	CO CATALYST	OTHER
FLORIDA POWER AND LIGHT	FL	PSD-FL-145	3/14/91	TURBINE, GAS, 4 EACH	240.00 MW	30.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
FLORIDA POWER AND LIGHT	FL	PSD-FL-145	3/14/91	TURBINE, OIL, 4 EACH	0.00	33.0000 PPM @ 15% O2	COMBUSTION CONTROL	BACT-PSD
NEVADA COGENERATION ASSOCIATES #2	NV	A391	1/17/91	COMBINED-CYCLE POWER GENERATION	85.00 MW POWER OUTPUT	39.9800 LBS/HR	CATALYTIC CONVERTER	BACT-PSD
NEVADA COGENERATION ASSOCIATES #1	NV	A360	1/17/91	COMBINED-CYCLE POWER GENERATION	85.00 MW TOTAL OUTPUT	39.9800 LBS/HR	CATALYTIC CONVERTER	BACT-PSD
NEWARK BAY COGENERATION PARTNERSHIP	NJ		11/1/90	TURBINE, KEROSENE FIRED	585.00 MMBTU/HR	0.0630 LB/MMBTU	CATALYTIC OXIDATION	BACT-PSD
NEWARK BAY COGENERATION PARTNERSHIP	NJ		11/1/90	TURBINE, NATURAL GAS FIRED	585.00 MMBTU/HR	0.0055 LB/MMBTU	CATALYTIC OXIDATION	BACT-PSD
TBG COGEN COGENERATION PLANT	NY	282400 5705 00001	8/5/90	GE LM2500 GAS TURBINE	214.90 MMBTU/HR	0.1810 LB/MMBTU	CATALYTIC OXIDIZER	BACT
SC ELECTRIC AND GAS COMPANY - HAGOOD STATION	SC	0560-0029	12/11/89	INTERNAL COMBUSTION TURBINE	110.00 MEGAWATTS	23.0000 LBS/HR	GOOD COMBUSTION PRACTICES	BACT-PSD
PEABODY MUNICIPAL LIGHT PLANT	MA	MBR-89-COM-032	11/30/89	TURBINE, 38 MW NATURAL GAS FIRED	412.00 MMBTU/HR	40.0000 PPM @ 15% O2	GOOD COMBUSTION PRACTICES	BACT-OTHE
MEGAN-RACINE ASSOCIATES, INC	NY	402201 0295 00001	8/5/89	GE LM5000-N COMBINED CYCLE GAS TURBINE	401.00 LB/MMBTU	0.0260 LB/MMBTU, 11 LB/HR	NO CONTROLS	BACT-OTHE
UNOCAL	CA	A/N 168294 AND 168295	7/18/89	TURBINE, GAS (SEE NOTES)	0.00	10.0000 PPM @ 15% O2	OXIDATION CATALYST	BACT-OTHE
KERN FRONT LIMITED	CA	S-1120-1-7	11/4/86	TURBINE, GAS, GENERAL ELECTRIC LM-2500	25.00 MW	669.1900 LB/D	OXIDATION CATALYST	BACT-OTHE
TOYOTA MOTOR MANUFACTURING U.S.A. INC.	KY	C-86-117	7/17/86	COMBUSTION, NATURAL GAS	0.00	0.0333 LB/MMBTU		BACT-PSD
UNION ELECTRIC CO	MO	0579-014 TO 0579-015	5/6/79	CONSTRUCTION OF A NEW OIL FIRED COMBUSTION	622.00 MM BTU/HR	463.0000 TYP		BACT-PSD
MILAGRO, WILLIAMS FIELD SERVICE	NM	PSD-NM-859-M-4		TURBINE/COGEN, NATURAL GAS (2)	900.00 MMCF/DAY	27.6000 PPM @ 15% O2		BACT-PSD
PILGRIM ENERGY CENTER	NY	472800 2054		(2) DUCT BURNER (EP #S 00001&2)	214.10 MMBTU/HR	0.1080 LB/MMBTU, 17.5 LB/HR		BACT-OTHE
PILGRIM ENERGY CENTER	NY	472800 2054		(2) WESTINGHOUSE W501DS TURBINES (EP #S 00001&2)	1400.00 MMBTU/HR	10.0000 PPM, 29.0 LB/HR		BACT-OTHE
LEDERLE LABORATORIES	NY	392400 0095		(2) GAS TURBINES (EP #S 00101&102)	110.00 MMBTU/HR	48.0000 PPM, 12.6 LB/HR		BACT-OTHE
BALTIMORE GAS & ELECTRIC - PERRYMAN PLANT	MD			TURBINE, 140 MW NATURAL GAS FIRED ELECTRIC	140.00 MW	20.0000 PPM @ 15% O2	GOOD COMBUSTION PRACTICES	BACT-PSD
COLORADO POWER PARTNERSHIP	CO	91MR933,1-2		TURBINES, 2 NAT GAS & 2 DUCT BURNERS	385.00 MMBTU/H EACH TURBIN	22.4000 PPM @ 15% O2		BACT-PSD

Table B-8. Direct and Indirect Capital Costs for CO Catalyst, General Electric Frame 7 Simple Cycle Combustion Turbine

Cost Component	Costs	Basis of Cost Component
<u>Direct Capital Costs</u>		
CO Associated Equipment	\$780,000	Vendor Quote
Flue Gas Ductwork	\$61,370	Vatavauk,1990
Instrumentation	\$78,000	10% of CO Associated Equipment
Sales Tax	\$46,800	6% of CO Associated Equipment
Freight	\$39,000	5% of CO Associated Equipment
<b>Total Direct Capital Costs (TDCC)</b>	<b>\$1,005,170</b>	
<u>Direct Installation Costs</u>		
Foundation and supports	\$80,414	8% of TDCC; OAQPS Cost Control Manual
Handling & Erection	\$140,724	14% of TDCC; OAQPS Cost Control Manual
Electrical	\$40,207	4% of TDCC; OAQPS Cost Control Manual
Piping	\$20,103	2% of TDCC; OAQPS Cost Control Manual
Insulation for ductwork	\$10,052	1% of TDCC; OAQPS Cost Control Manual
Painting	\$10,052	1% of TDCC; OAQPS Cost Control Manual
Site Preparation	\$5,000	Engineering Estimate
Buildings	\$0	
<b>Total Direct Installation Costs (TDIC)</b>	<b>\$306,551</b>	
<b>Total Capital Costs</b>	<b>\$1,311,721</b>	Sum of TDCC, TDIC and RCC
<u>Indirect Costs</u>		
Engineering	\$100,517	10% of TDCC; OAQPS Cost Control Manual
Construction and Field Expense	\$50,258	5% of TDCC; OAQPS Cost Control Manual
Contractor Fees	\$100,517	10% of TDCC; OAQPS Cost Control Manual
Start-up	\$20,103	2% of TDCC; OAQPS Cost Control Manual
Performance Tests	\$10,052	1% of TDCC; OAQPS Cost Control Manual
Contingencies	\$30,155	3% of TDCC; OAQPS Cost Control Manual
<b>Total Indirect Capital Cost (TInDC)</b>	<b>\$311,603</b>	
<b>Total Direct, Indirect and Capital Costs (TDICC)</b>	<b>\$1,623,323</b>	Sum of TCC and TInCC
<u>Mass Flow of Combustion Turbine</u>		
	3,600,000 lb/hr	"F"

Table B-9. Annualized Cost for CO Catalyst, General Electric Frame F Simple Cycle Combustion Turbine

Cost Component	Cost	Basis of Cost Estimate
<u>Direct Annual Costs</u>		
Operating Personnel	\$6,240	8 hours/week at \$15/hr
Supervision	\$936	15% of Operating Personnel; OAQPS Cost Control Manual
Catalyst Replacement	\$200,000	3 year catalyst life; base on Vendor Budget Quote
Inventory Cost	\$21,960	Capital Recovery (10.98%) for 1/3 catalyst
Contingency	\$6,874	3% of Direct Annual Costs
<b>Total Direct Annual Costs (TDAC)</b>	<b>\$236,010</b>	
<u>Energy Costs</u>		
Heat Rate Penalty	\$83,747	0.2% of MW output; EPA, 1993 (Page 6-20) and \$3/mmBtu addl fuel costs
<b>Total Energy Costs (TDEC)</b>	<b>\$83,747</b>	
<u>Indirect Annual Costs</u>		
Overhead	\$4,306	60% of Operating/Supervision Labor
Property Taxes	\$16,233	1% of Total Capital Costs
Insurance	\$16,233	1% of Total Capital Costs
Annualized Total Direct Capital	\$178,241	10.98% Capital Recovery Factor of 7% over 15 yrs times sum of TDACC
<b>Total Indirect Annual Costs</b>	<b>\$215,013</b>	
<b>Total Annualized Costs</b>	<b>\$534,770</b>	Sum of TDAC, TEC and TIAC
<b>Cost Effectiveness</b>	<b>\$8,396</b>	Simple Cycle Combustion Turbine
	<b>\$12,869</b>	Net Emission Reduction

Table B-10. Comparison of Alternative BACT Control Technologies for CO on Simple-cycle Unit

	Alternative BACT Control Technologies	
	DLN Only	DLN/WI with OC
Technical Assessment	Feasible	Available, Feasible and Demonstrated
Economic Impact <sup>a</sup>		
Capital Costs	included	\$1,623,323
Annualized Costs	included	\$534,770
Cost Effectiveness		
CO Removed (per ton of CO)	NA	\$8,396
CO Removed (per ton of total pollutants)	NA	\$12,869
Environmental Impact <sup>b</sup>		
Total CO (TPY)	70.8	7.1
CO Reduction (TPY)	NA	(63.7)
PM Emissions (TPY)	0	20.8
Secondary Emissions (TPY)	0	1.3
Net Emission Reduction (TPY)	NA	(41.6)
Energy Impacts <sup>c</sup>		
Energy Use (kWh/yr)	0	1,182,432
Energy Use (mmBtu/yr) at 10,000 Btu/kWh	0	11,452
Energy Use (mmcf/yr) at 1,000 Btu/cf for natural gas	0	11

<sup>a</sup> See Tables B-8 and B-9 for detailed development of capital costs (including recurring costs) and annualized costs.

<sup>b</sup> See emission data presented in Table B-11.

<sup>c</sup> Energy impacts are estimated due to the lost energy from heat rate penalty for 3,390 hours per year. Lost energy is based on 0.2 percent of 174.4 MW.

Table B-11. Maximum Potential Incremental Emissions (TPY) with an Oxidation Catalyst for Simple Cycle Unit

Pollutants	Incremental Emissions (tons/year) of SCR		Total
	Primary	Secondary	
Particulate	20.83	0.04	20.87
Sulfur Dioxide		0.02	0.02
Nitrogen Oxides		0.76	0.76
Carbon Monoxide	-63.70	0.46	-63.24
Volatile Organic Compounds		0.03	0.03
	Total:		
Carbon Dioxide (additional from gas firing)	-42.86	1.31	-41.56
		725.28	725.28

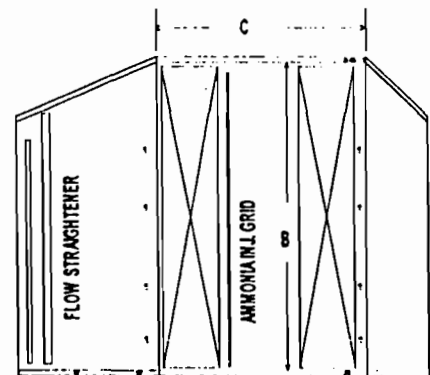
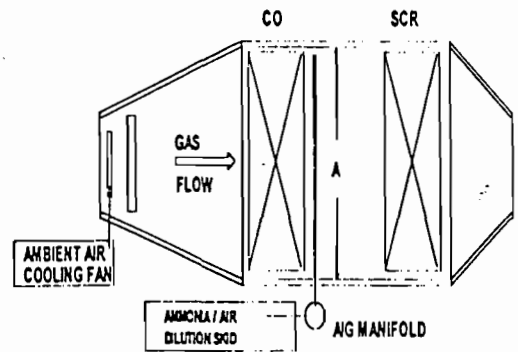
Basis:

Lost Energy (mmBtu/year)	11,452
Secondary Emissions (lb/mmBtu): Assumes natural gas firing in NOx controlled steam unit.	
Particulate	0.0072
Sulfur Dioxide	0.0027
Nitrogen Oxides w/LNB	0.1333
Carbon Monoxide	0.0800
Volatile Organic Compounds	0.0052

Reference: Table 1.4-1 and 1.4-2, AP-42, Version 2/98



Dimensions / Sketch: Simple Cycle  
CO and SCR - w/ ambient cooling  
Required Cross Sectional Area  
Inside Liner Width x Inside Liner Height  
(A x B) sq. ft.  
Reactor Depth (C) 15'-0"



# ENGELHARD

Golder Assoc.  
 Westinghouse 501D and GE 7FA - Simple and Combined Cycle  
 CAMET® CO Oxidation Catalyst System  
 VNX™ / ZNX™ SCR Catalyst System  
 Engelhard Budgetary Proposal EPB99639  
 December 13, 1999

## GE 7FA - Simple Cycle

ASSUMED AMBIENT	59	59
GIVEN TURBINE EXHAUST TEMPERATURE, F	1,100	1,100
GIVEN TURBINE EXHAUST FLOW, lb/hr	3,900,000	4,080,000
ASSUMED TURBINE EXHAUST GAS ANALYSIS, % VOL.		
N2	75.23	71.63
O2	12.61	11.04
CO2	3.63	5.20
H2O	7.60	11.20
Ar	0.93	0.93
AMBIENT AIR FLOW, lb/hr	332,949	348,316
TOTAL FLOW - TURBINE EXHAUST + AMBIENT - lb/hr	4,232,949	4,428,316
AMBIENT + EXHAUST GAS ANALYSIS, % VOL.		
N2	75.70	72.37
O2	13.09	11.64
CO2	3.35	4.80
H2O	7.01	10.33
Ar	0.86	0.86
CALCULATED AIR + GAS MOL. WT.	28.48	28.32
GIVEN: TURBINE CO, ppmvd	9.0	20.0
CALC.: TURBINE CO, lb/hr	31.9	71.7
GIVEN: TURBINE NOx, ppmvd @ 15% O2	9.0	42.0
CALC.: TURBINE NOx, lb/hr	64.5	355.2
CALC.: CO, ppmvd @ 15% O2 - AT CATALYST FACE	7.1	13.6
CALC.: NOx, ppmvd @ 15% O2 - AT CATALYST FACE	8.8	41.0
FLUE GAS TEMP. @ SCR CATALYST, F	1,025	1,025
DESIGN REQUIREMENTS		
CO CATALYST CO CONVERSION, %	90%	90%
SCR CATALYST NOx OUT, ppmvd @ 15% O2	3.5	ADVISE
NH3 SLIP, ppmvd @ 15% O2	9	12
SCR PRESSURE DROP, 4.0"WG - Nom.		
GUARANTEED PERFORMANCE DATA		
CO CONVERSION - % Min.	90.0%	90.0%
CO OUT, ppmvd @ 15% O2	0.7	1.4
CO OUT, lb/hr	3.2	7.2
CO PRESSURE DROP	2.2	2.4
SCR CATALYST NOx CONVERSION, % - Min.	61.1%	61.1%
NOx OUT, lb/hr - Max.	25.1	138.1
NOx OUT, ppmvd@15%O2 - Max.	3.4	16.0
EXPECTED AQUEOUS NH3 (28% SOL.) FLOW, lb/hr	139	424
NH3 SLIP, ppmvd@15%O2 - Max.	9	12
SCR PRESSURE DROP, "WG - Max.	4.2	4.4
REQUIRED CROSS SECTION - INSIDE LINER - A x B, sq ft	1650.0	
CO SYSTEM	\$843,000	
REPLACEMENT CO CATALYST MODULES	\$643,000	
SCR SYSTEM	\$2,835,000	
REPLACEMENT SCR CATALYST MODULES	\$1,479,000	



**APPENDIX C**

**SUMMARY OF THE CALPUFF MODEL DESCRIPTION AND ASSUMPTIONS USED  
IN THE PSD CLASS I MODELING ANALYSES**

## C.0 SUMMARY OF CALPUFF MODEL DESCRIPTION AND ASSUMPTIONS USED IN THE PSD CLASS I MODELING ANALYSES

### C.1 INTRODUCTION

As part of the new source review requirements under Prevention of Significant Deterioration (PSD) regulations, new sources are required to address air quality impacts at PSD Class I areas.

As part of the PSD analysis report submitted to the Florida Department of Environmental Protection (DEP), the air quality impacts due to the potential emissions of the Peace River Station Project are required to be addressed at the PSD Class I area of the Chassahowitzka National Wildlife Area (NWA). The Chassahowitzka NWA is located approximately 124 km north-northwest of the Project site and is the nearest Class I area to the Project. Other PSD Class I areas are located more than 200 km from the Project.

The evaluation of air quality impacts are not only concerned with determining compliance with PSD Class I increments but also assessing a source's impact on Air Quality Related Values (AQRVs), such as regional haze. Further, compliance with PSD Class I increments can be evaluated by determining if the source's impacts are less than the proposed U.S. Environmental Protection Agency (EPA) Class I significant impact levels. The significant impact levels are threshold levels that are used to determine the type of air impact analyses needed for the project. If the new source's impacts are predicted to be less than significant, then the source's impacts are assumed not to have a significant adverse affect on air quality and additional modeling with other sources is not required. However, if the source's impacts are predicted to be greater than the significant impact levels, additional modeling with other sources is required to demonstrate compliance with Class I increments.

Currently there are several air quality modeling approaches recommended by the Interagency Workgroup on Air Quality Models (IWAQM) to perform these analyses. The IWAQM consists of EPA and Federal Land Managers (FLM) of Class I areas who are responsible for ensuring that AQRVs are not adversely impacted by new and existing sources. These recommendations have been summarized in two documents:

- *Interagency Workgroup on Air Quality Models (IWAQM) Phase 1 Report: Interim Recommendations for Modeling Long Range Transport and Impacts on Regional Visibility* (EPA, 1993), referred to as the Phase 1 report; and
- *Interagency Workgroup on Air Quality Models (IWAQM), Phase 2 Summary Report and Recommendations for Modeling Long Range Transport Impacts* (EPA, 1998), referred to as the Phase 2 report.

The recommended modeling approaches from these documents are as follows:

- Phase 1 report: screening analysis (Level 1)
- Phase 2 report: screening analysis
- Phase 2 report: refined analysis

For the Project, air quality analyses were performed that assess the Project's impacts in the PSD Class I area of the Chassahowitzka NWA using the refined approach from the Phase 2 report for:

- Significant impact analysis; and
- Regional haze analysis.

The refined analysis approach was used instead of the screening analysis approach since the air quality impacts are based on generally more realistic assumptions, include more detailed meteorological data, and are estimated at locations at the Class I area.

## **C.2 GENERAL AIR MODELING APPROACH**

The general modeling approach was based on using the Industrial Source Complex Short-term model (ISCST3, Version 99155) and the long-range transport model, California Puff model (CALPUFF, Version 5.0). The ISCST3 model is applicable for estimating the air quality impacts in areas that are within 50 km from a source. At distances beyond 50 km, the ISCST3 model is considered to overpredict air quality impacts because it is a steady-state model. At those distances, the CALPUFF model is recommended for use. Recently, the FLM have requested that air quality impacts, such as for regional haze, for a source located more than 50 km from a Class I area be predicted using the CALPUFF model. The Florida DEP has also recommended that the CALPUFF model be used to assess if the source has a significant impact at a Class I area located

beyond 50 km from the source. As a result, a significant impact and regional haze analyses were performed using the CALPUFF model to assess the Project's impacts at the Chassahowitzka NWA.

The methods and assumptions used in the CALPUFF model were based on the latest recommendations for a screening analysis as presented in the *Interagency Workgroup on Air Quality Models (IWAQM), Phase 2 Summary Report and Recommendations for Modeling Long Range Transport Impacts* (EPA, 1998).

Based on discussions with DEP, the ISCST3 model can be used to determine the "worst-case" operating load and ambient temperature that produces a source's maximum impact at a Class I area. Based on that analysis, air quality impacts can then be predicted with the CALPUFF model using the "worst-case" operating scenario to compare the source's impacts to Class I significant impact levels and potential contribution to regional haze. For this Project, the ISCST3 model was used to determine the "worst-case" operating scenario that was then considered in the CALPUFF model. The methods and assumptions used in the ISCST3 were based on those presented in Section 6.0 of the PSD report.

A regional haze analysis was performed to determine the affect that the Project's emissions will have on background regional haze levels at the Chassahowitzka NWA. In the regional haze analysis, the change in visual range, as calculated by a deciview change, was estimated for the Project in accordance with the IWAQM recommendations. Based on those recommendations, the CALPUFF model is used to predict the maximum 24-hour average sulfate ( $\text{SO}_4$ ), nitrate ( $\text{NO}_3$ ), and fine particulate ( $\text{PM}_{10}$ ) concentrations as well as ammonium sulfate ( $(\text{NH}_4)_2\text{SO}_4$ ) and ammonium nitrate ( $\text{NH}_4\text{NO}_3$ ) concentrations. The change in visibility due to a source, estimated as a percentage, is then calculated based on the change from background data.

The following sections present the methods and assumptions used to assess the refined significant impact and regional haze analyses performed for the Project. The results of these analyses are presented in Sections 6.0 and 7.0 of the PSD report.

### **C.3 MODEL SELECTION AND SETTINGS**

The California Puff (CALPUFF, version 5.0) air modeling system was used to model to assess the Project's impacts at the PSD Class I area for comparison to the PSD Class I significant impact levels and to the regional haze visibility criteria. CALPUFF is a non-steady state Lagrangian Gaussian puff long-range transport model that includes algorithms for building downwash effects as well as chemical transformations (important for visibility controlling pollutants), and wet/dry deposition. The CALPUFF meteorological and geophysical data preprocessor (CALMET, Version 5), a preprocessor to CALPUFF, is a diagnostic meteorological model that produces a three-dimensional field of wind and temperature and a two-dimensional field of other meteorological parameters. CALMET was designed to process raw meteorological, terrain and land-use databases to be used in the air modeling analysis. The CALPUFF modeling system uses a number of FORTRAN preprocessor programs that extract data from large databases and converts the data into formats suitable for input to CALMET. The processed data produced from CALMET was input to CALPUFF to assess the pollutant specific impact. Both CALMET and CALPUFF were used in a manner that is recommended by the IWAQM Phase 2 Report (EPA, 1998).

#### **C.3.1 CALPUFF MODEL APPROACHES AND SETTINGS**

The IWAQM has recommended approaches for performing a Phase 2 refined modeling analyses that are presented in Table C-1. These approaches involve use of meteorological data, selection of receptors and dispersion conditions, and processing of model output.

The specific settings used in the CALPUFF model are presented in Table C-2.

#### **C.3.2 EMISSION INVENTORY AND BUILDING WAKE EFFECTS**

The CALPUFF model included the Project's emission, stack, and operating data as well as building dimensions to account for the effects of building-induced downwash on the emission sources. Dimensions for all significant building structures were processed with the Building Profile Input Program (BPIP), Version 95086, and were included in the CALPUFF model input. The PSD Analysis Report presents a listing of the Project's emissions and structures included in the analysis.

#### **C.4 RECEPTOR LOCATIONS**

For the refined analyses, pollutant concentrations were predicted in an array of 13 discrete receptors located at the CNWR area. These receptors are the same as those used in the PSD Class I analysis performed for the PSD Analysis Report.

#### **C.5 METEOROLOGICAL DATA**

##### **C.5.1 REFINED ANALYSIS**

CALMET was used to develop the gridded parameter fields required for the refined modeling analyses. The follow sections discuss the specific data used and processed in the CALMET model.

##### **C.5.2 CALMET SETTINGS**

The CALMET settings contained in Table C-3 were used for the refined modeling analysis. With the exception of hourly precipitation data files, all input data files needed for CALMET were developed by the FDEP staff.

2988893.426  
251915.432

##### **C.5.3 MODELING DOMAIN**

A rectangular modeling domain extending 250 km in the east-west (x) direction and 280 km in the north-south (y) direction was used for the refined modeling analysis. The extent of the modeling domain was selected by the Florida DEP staff for predicting impacts at the Chassahowitzka NWA. The southwest corner of the domain is the origin and is located at 27 degrees north latitude and 83.5 degrees west longitude. This location is in the Gulf of Mexico approximately 110 km west of Venice, Florida. For the processing of meteorological and geophysical data, the domain contains 25 grid cells in the x-direction and 28 grid cells in the y-direction. The domain grid resolution is 10 km. The air modeling analysis was performed in the UTM coordinate system.

##### **C.5.4 MESOSCALE MODEL – GENERATION 4 (MM4) DATA**

Pennsylvania State University in conjunction with the NCAR Assessment Laboratory developed the MM4 data set, a prognostic wind field or "guess" field, for the United States. The hourly meteorological variables used to create this data set (wind, temperature, dew point depression,

and geopotential height for eight standard levels and up to 15 significant levels) are extensive and only allow for one data base set for the year 1990. The analysis used the MM4 data to initialize the CALMET wind field. The MM4 data have a horizontal spacing of 80 km and are used to simulate atmospheric variables within the modeling domain.

The MM4 subset domain was provided by FDEP and consisted of a 6 x 6- cell rectangle, with 80 km grid resolution, extending from the MM4 grid points (49,10) to (54, 15). These data were processed to create a MM4.DAT file, for input to the CALMET model.

The MM4 data set used in the CALMET, although advanced, lacks the fine detail of specific temporal and spatial meteorological variables and geophysical data. These variables were processed into the appropriate format and introduced into the CALMET model through the additional data files obtained from the following sources.

#### **C.5.5 SURFACE DATA STATIONS AND PROCESSING**

The surface station data processed for the CALPUFF analyses consisted of data from five NWS stations or Federal Aviation Administration (FAA) Flight Service stations for Gainesville, Tampa, Daytona Beach, Vero Beach, Fort Myers and Orlando. A summary of the surface station information and locations are presented in Table C-4. The surface station parameters include wind speed, wind direction, cloud ceiling height, opaque cloud cover, dry bulb temperature, relative humidity, station pressure, and a precipitation code that is based on current weather conditions. The surface station data were processed by FDEP into a SURF.DAT file format for CALMET input.

Because the modeling domain extends largely over water, C-Man station data from Venice was obtained. These data were processed by Florida DEP into an over-water surface station format (i.e., SEA\*.DAT) for input to CALMET. The over-water station data include wind direction, wind speed and air temperature.

### **C.5.6 UPPER AIR DATA STATIONS AND PROCESSING**

The analysis included three upper air NWS stations located in Ruskin, Apalachicola, and West Palm Beach. Data for each station were obtained from the Florida DEP in a format for CALMET input.

The data and locations for the upper air stations are presented in Table C-4.

### **C.5.7 PRECIPITATION DATA STATIONS AND PROCESSING**

Precipitation data were processed from a network of hourly precipitation data files collected from primary and secondary NWS precipitation-recording stations located within the latitude and longitudinal limits of the modeling domain. Data for 14 stations were obtained in NCDC TD-3240 variable format and converted into a fixed-length format. The utility programs PEXTRACT and PMERGE were then used to process the data into the format for the PRECIP.DAT file that is used by CALMET. A listing of the precipitation stations used for the modeling analysis is presented in Table C-5.

### **C.5.8 GEOPHYSICAL DATA PROCESSING**

The land-use and terrain information data were developed by the FDEP for the modeling domain and were provided in a GEO.DAT file format for input to CALMET. Terrain elevations for each grid cell of the modeling domain were obtained from Digital Elevation Model (DEM) files obtained from US Geographical Survey (USGS). The DEM data was extracted for the modeling domain grid using the utility extraction program LCELEV. Land-use data were obtained from the USGS GIS.DAT which is based on the ARM3 data. The resolution of the GIS.DAT file is one-eighth of a degree in the east-west direction and one-twelfth of a degree in the north-south direction. Land-use values for the domain grid were obtained with the utility program CAL-LAND. Other parameters processed for the modeling domain by CAL-LAND include surface roughness, surface Albedo, Bowen ratio, soil heat flux, and leaf index field. The land-use parameter values were based on annual averaged values.



Table C-1. IWAQM Phase 2 Refined Modeling Analyses Recommendations<sup>a</sup>

Model Input/Output	Description
Meteorology	Use CALMET (minimum 6 to 10 layers in the vertical; top layer must extend above the maximum mixing depth expected); horizontal domain extends 50 to 80 km beyond outer receptors and sources being modeled; terrain elevation and land-use data is resolved for the situation.
Receptors	Within Class I area(s) of concern; obtain regulatory concurrence on coverage.
Dispersion	<ol style="list-style-type: none"> <li>1. CALPUFF with default dispersion settings.</li> <li>2. Use MESOPUFF II chemistry with wet and dry deposition.</li> <li>3. Define background values for ozone and ammonia for area.</li> </ol>
Processing	<ol style="list-style-type: none"> <li>1. For PSD increments: Use highest, second highest 3-hour and 24-hour average SO<sub>2</sub> concentrations; highest, second highest 24-hour average PM<sub>10</sub> concentrations; and highest annual average SO<sub>2</sub>, PM<sub>10</sub> and NO<sub>2</sub> concentrations.</li> <li>2. For haze: process the 24-hour average SO<sub>4</sub>, NO<sub>3</sub> and HNO<sub>3</sub> values; compute a 24-hour average relative humidity factor (f(RH)) for the day during which the highest concentration was predicted for each species; calculate extinction coefficients for each species; and compute percent change in extinction using the FLM supplied background extinction.</li> </ol>

<sup>a</sup> IWAQM Phase 2 Summary Report and Recommendations for Modeling Long Range Transport Impacts (EPA, 1998)

Table C-2. CALPUFF Model Settings

Parameter	Setting
Pollutant Species	SO <sub>2</sub> , SO <sub>4</sub> , NO <sub>x</sub> , HNO <sub>3</sub> , and NO <sub>3</sub> , and PM <sub>10</sub>
Chemical Transformation	MESOPUFF II scheme
Deposition	Include both dry and wet deposition, plume depletion
Meteorological/Land Use Input	PCRAMMET (enhanced) for the screening analysis; CALMET for the refined analysis
Plume Rise	Transitional, Stack-tip downwash, Partial plume penetration
Dispersion	Puff plume element, PG /MP coefficients, rural mode, ISC building downwash scheme
Terrain Effects	Partial plume path adjustment
Output	Create binary concentration file including output species for SO <sub>4</sub> , NO <sub>3</sub> and PM <sub>10</sub>
Model Processing	Highest predicted 24-hour SO <sub>4</sub> , NO <sub>3</sub> and PM <sub>10</sub> concentrations for year
Background Values <sup>a</sup>	Ozone: 80 ppb; Ammonia: 10 ppb

<sup>a</sup> Recommended values by the Florida DEP.

Table C-3. CALMET Settings

Parameter	Setting
Horizontal Grid Dimensions	250 by 280 km, 10 km grid resolution
Vertical Grid	9 layers
Weather Station Data Inputs	6 surface, 3 upper air, 14 precipitation stations
Wind model options	Diagnostic wind model, no kinematic effects
Prognostic wind field model	MM4 data, 80 km resolution, 6 x 6 grid, used for wind field initialization
Output	Binary hourly gridded meteorological data file for CALPUFF input

Table C-4. Surface and Upper Air Stations Used in the CALPUFF Analysis

Station Name	Station Symbol	WBAN Number	UTM Coordinates			Anemometer Height (m)
			Easting (km)	Northing (km)	Zone	
<b>Surface Stations</b>						
Tampa	TPA	12842	349.20	3094.25	17	6.7
Daytona Beach	DAB	12834	495.14	3228.05	17	9.1
Orlando	ORL	12815	468.96	3146.88	17	10.1
Gainesville	GNV	12816	377.40	3284.12	17	6.7
Vero Beach	VER	12843	557.52	3058.36	17	6.7
Fort Myers	FMY	12835	413.65	2940.38	17	6.1
<b>Upper Air Stations</b>						
Ruskin	TBW	12842	349.20	3094.28	17	NA
West Palm Beach	PBI	12844	587.87	2951.42	17	NA
Apalachicola	AQQ	12832	110.00 <sup>a</sup>	3296.00	16	NA

<sup>a</sup> Equivalent coordinate for Zone 17; Zone 16 coordinate is 690.22 km.

Table C-5. Hourly Precipitation Stations Used in the CALPUFF Analysis

Station Name (Florida)	Station Number	UTM Coordinates		
		Easting (km)	Northing (km)	Zone
Brooksville 7 SSW	81048	358.03	3149.55	17
Daytona Beach WSO AP	82158	495.14	3228.09	17
Deland 1 SSE	82229	470.78	3209.66	17
Inglis-3 E	84273	342.63	3211.65	17
Lakeland	84797	409.87	3099.18	17
Lisbon	85076	423.59	3193.26	17
Lynne	85237	409.26	3230.30	17
Orlando WSO McCoy	86628	468.99	3146.88	17
Parrish	86880	366.99	3054.39	17
Saint Leo	87851	376.48	3135.09	17
St. Petersburg	87886	339.04	3072.21	17
Tampa WSCMO AP	88788	349.17	3094.25	17
Venice	89176	357.59	2998.18	17
Venus	89184	466.756	2996.09	17

**APPENDIX D**

**BUILDING DOWNWASH INFORMATION FROM BPIP**

'DECKER. ORIENTED NORTH AS PLANT NORTH 04/18/00'

'ST'

'METERS' 1.00

'UTMN' 0.0

8

'CT1'	1	0
	4	6.706
	-34.0	-24.5
	-43.1	-24.5
	-43.1	-11.7
	-34.0	-11.7

'CT2'	1	0
	4	6.706
	5.1	-24.5
	-4.0	-24.5
	-4.0	-11.7
	5.1	-11.7

'CT3'	1	0
	4	6.706
	44.9	-24.5
	35.7	-24.5
	35.7	-11.7
	44.9	-11.7

'AIR1'	1	0
	4	14.326
	-49.3	-30.6
	-60.3	-30.6
	-60.3	-19.6
	-49.3	-19.6

'AIR2'	1	0
	4	14.326
	-10.2	-30.6
	-21.2	-30.6
	-21.2	-19.6
	-10.2	-19.6

'AIR3'	1	0
	4	14.326
	28.9	-30.6
	17.9	-30.6
	17.9	-19.6
	28.9	-19.6

'TANK1'	1	0
	8	14.630
	-108.8	-6.1
	-112.2	2.0
	-108.8	10.2
	-99.2	13.6
	-91.1	10.2
	-87.7	2.0
	-91.1	-6.1
	-98.6	-10.2

'TANK2'	1	0
	8	14.630
	-108.8	-37.4
	-112.2	-28.9
	-108.8	-20.4
	-99.2	-17.0
	-91.1	-20.4
	-87.7	-28.9
	-91.1	-37.4
	-98.6	-41.5

3

'CT1'	0.0	18.288	-39.08	0.0
'CT2'	0.0	18.288	0.0	0.0
'CT3'	0.0	18.288	39.08	0.0

0

BPIP (Dated: 95086)

DATE : 04/18/00  
 TIME : 11:50:04  
 DECKER. 04/18/00

=====  
 BPIP PROCESSING INFORMATION:  
 =====

The ST flag has been set for processing for an ISCST2 run.

Inputs entered in METERS will be converted to meters using a conversion factor of 1.0000. Output will be in meters.

UTMP is set to UTMN. The input is assumed to be in a local X-Y coordinate system as opposed to a UTM coordinate system. True North is in the positive Y direction.

Plant north is set to 0.00 degrees with respect to True North.

DECKER. 04/18/00

PRELIMINARY\* GEP STACK HEIGHT RESULTS TABLE  
 (Output Units: meters)

Stack Name	Stack Height	Stack-Building Base Elevation Differences	GEP** EQN1	Preliminary* GEP Stack Height Value
CT1	18.29	0.00	36.58	65.00
CT2	18.29	0.00	35.82	65.00
CT3	18.29	0.00	35.82	65.00

\* Results are based on Determinants 1 & 2 on pages 1 & 2 of the GEP Technical Support Document. Determinant 3 may be investigated for additional stack height credit. Final values result after Determinant 3 has been taken into consideration.

\*\* Results were derived from Equation 1 on page 6 of GEP Technical Support Document. Values have been adjusted for any stack-building base elevation differences.

Note: Criteria for determining stack heights for modeling emission limitations for a source can be found in Table 3.1 of the GEP Technical Support Document.

BPIP (Dated: 95086)

DATE : 04/18/00  
 TIME : 11:50:04  
 DECKER. 04/18/00

BPIP output is in meters

SO BUILDHGT CT1	14.33	14.33	14.33	14.33	14.63	14.63
SO BUILDHGT CT1	14.63	14.63	14.63	14.63	0.00	14.33
SO BUILDHGT CT1	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT CT1	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT CT1	0.00	0.00	0.00	0.00	14.33	14.33
SO BUILDHGT CT1	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID CT1	12.74	14.10	15.03	15.50	24.40	23.57
SO BUILDWID CT1	23.32	23.54	23.80	23.33	0.00	15.03
SO BUILDWID CT1	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID CT1	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID CT1	0.00	0.00	0.00	0.00	14.10	15.03
SO BUILDWID CT1	15.50	15.50	15.03	14.10	11.18	9.10



SO BUILDHGT CT2	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT CT2	14.33	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT CT2	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT CT2	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT CT2	0.00	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT CT2	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID CT2	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID CT2	14.10	0.00	0.00	0.00	0.00	15.03
SO BUILDWID CT2	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID CT2	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID CT2	0.00	0.00	0.00	0.00	0.00	15.03
SO BUILDWID CT2	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDHGT CT3	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT CT3	14.33	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT CT3	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT CT3	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT CT3	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT CT3	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID CT3	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID CT3	14.10	0.00	0.00	0.00	0.00	0.00
SO BUILDWID CT3	0.00	15.28	14.37	13.02	11.28	9.20
SO BUILDWID CT3	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID CT3	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID CT3	0.00	15.28	14.37	13.02	11.28	9.20

**APPENDIX E**

**SUMMARY OF ISCST AND CALPUFF COMPUTER MODEL INPUT AND OUTPUT  
FILES (EXAMPLE FILES FOR FIRST YEAR OF MODELING)**

Table E-1. Maximum Pollutant Concentrations Predicted for One Combustion Turbine in Simple Cycle Operation Firing Natural Gas and Distillate Fuel Oil  
Based on Modeled Generic Emission Rate

Pollutant	Maximum Emission Rates (lb/hr) by Operating Load and Air Temperature						Averaging Time	Maximum Predicted Concentrations (ug/m <sup>3</sup> ) by Operating Load and Air Temperature (1)					
	Base Load		75% Load		50% Load			Base Load		75% Load		50% Load	
	32°F	95°F	32°F	95°F	32°F	95°F		32°F	95°F	32°F	95°F	32°F	95°F
<b>Natural Gas</b>													
Generic (10 g/s)	79.37	79.37	79.37	79.37	79.37	79.37	Annual	0.0174	0.0187	0.0203	0.0221	0.0258	0.0273
							24-Hour	0.2193	0.2360	0.2534	0.2730	0.3090	0.3320
							8-Hour	0.4775	0.5041	0.5441	0.5845	0.6643	0.7884
							3-Hour	1.0096	1.0193	1.0343	1.2192	1.7164	1.7339
							1-Hour	2.0697	2.1964	2.3758	2.5533	2.8763	3.0785
SO <sub>2</sub>	10.4	9.3	8.6	7.3	6.5	5.6	Annual	0.00228	0.00218	0.00220	0.00204	0.00211	0.00192
							24-Hour	0.0288	0.0275	0.0274	0.0252	0.0253	0.0233
							3-Hour	0.133	0.119	0.112	0.113	0.140	0.122
PM10	11.0	11.0	11.0	11.0	11.0	11.0	Annual	0.0024	0.0026	0.0028	0.0031	0.0036	0.0038
							24-Hour	0.0304	0.0327	0.0351	0.0378	0.0428	0.0460
NO <sub>x</sub>	71.9	63.9	59.3	50.6	44.7	38.5	Annual	0.016	0.015	0.015	0.014	0.015	0.013
CO	35.9	31.4	28.5	25.3	25.2	23.6	8-Hour	0.22	0.20	0.20	0.19	0.21	0.23
							1-Hour	0.93	0.87	0.85	0.81	0.91	0.92
<b>Distillate Fuel Oil</b>													
Generic (10 g/s)	79.37	79.37	79.37	79.37	79.37	79.37	Annual	0.0169	0.0179	0.0199	0.0216	0.0253	0.0275
							24-Hour	0.2147	0.2241	0.2495	0.2681	0.3049	0.3322
							8-Hour	0.4671	0.4886	0.5352	0.5743	0.6554	0.7890
							3-Hour	1.0056	1.0134	1.0308	1.2157	1.7114	1.7358
							1-Hour	2.0190	2.0770	2.3380	2.5372	2.8361	3.0805
SO <sub>2</sub>	106.9	96.2	87.2	75.3	64.9	56.2	Annual	0.023	0.022	0.022	0.020	0.021	0.019
							24-Hour	0.29	0.27	0.27	0.25	0.25	0.24
							3-Hour	1.35	1.23	1.13	1.15	1.40	1.23
PM10	22.0	22.0	22.0	22.0	22.0	22.0	Annual	0.0047	0.0050	0.0055	0.0060	0.0070	0.0076
							24-Hour	0.060	0.062	0.069	0.074	0.085	0.092
NO <sub>x</sub>	352.1	316.9	287.3	248.2	213.9	185.2	Annual	0.075	0.071	0.072	0.067	0.068	0.064
CO	72.6	63.5	56.9	50.0	51.0	47.8	8-Hour	0.43	0.39	0.38	0.36	0.42	0.48
							1-Hour	1.85	1.66	1.68	1.60	1.82	1.86

(1) Concentrations are based on highest predicted concentrations using five years of meteorological for 1987 to 1991 of surface and upper air data from the National Weather Service stations at Tampa International Airport and Ruskin, respectively.

Pollutant concentrations were based on a modeled or generic concentration predicted using a modeled emission rate of 79.37 lb/hr (10 g/s). Specific pollutant concentrations were estimated by multiplying the modeled concentration (at 10 g/s) by the ratio of the specific pollutant emission rate to the modeled emission rate of 10 g/s.

Table E-2. Maximum Pollutant Concentrations Predicted for One Combustion Turbine Firing Natural Fuel and Distillate Fuel Oil in Simple-Cycle Operation at the PSD Class I Area of the Chassahowitzka NWA Based on Modeled Generic Emission Rate

Pollutant	Maximum Emission Rates (lb/hr) by Operating Load and Air Temperature						Averaging Time	Maximum Predicted Concentrations (ug/m <sup>3</sup> ) by Operating Load and Air Temperature (1)					
	Base Load		75% Load		50% Load			Base Load		75% Load		50% Load	
	32°F	95°F	32°F	95°F	32°F	95°F		32°F	95°F	32°F	95°F	32°F	95°F
<b>Natural Gas</b>													
Generic (10 g/s)	79.37	79.37	79.37	79.37	79.37	79.37	Annual	0.0031	0.0032	0.0035	0.0037	0.0041	0.0042
							24-Hour	0.0477	0.0495	0.0575	0.0616	0.0685	0.0711
							8-Hour	0.1449	0.1489	0.1549	0.1666	0.1873	0.1951
							3-Hour	0.3092	0.3185	0.3320	0.3448	0.3692	0.3815
							1-Hour	0.5884	0.6103	0.6424	0.6734	0.7260	0.7451
SO <sub>2</sub>	10.4	9.3	8.6	7.3	6.5	5.6	Annual	0.00040	0.00038	0.00037	0.00034	0.00034	0.00030
							24-Hour	0.0063	0.0058	0.0062	0.0057	0.0056	0.0050
							3-Hour	0.041	0.037	0.036	0.032	0.030	0.027
PM10	11.0	11.0	11.0	11.0	11.0	11.0	Annual	0.0004	0.0004	0.0005	0.0005	0.0006	0.0006
							24-Hour	0.0066	0.0069	0.0080	0.0085	0.0095	0.0099
NO <sub>x</sub>	71.9	63.9	59.3	50.6	44.7	38.5	Annual	0.003	0.003	0.003	0.002	0.002	0.002
<b>Distillate Fuel Oil</b>													
Generic (10 g/s)	79.37	79.37	79.37	79.37	79.37	79.37	Annual	0.0030	0.0031	0.0034	0.0037	0.0041	0.0042
							24-Hour	0.0470	0.0485	0.0566	0.0606	0.0677	0.0714
							8-Hour	0.1433	0.1466	0.1533	0.1636	0.1849	0.1960
							3-Hour	0.3054	0.3131	0.3290	0.3417	0.3655	0.3829
							1-Hour	0.5795	0.5973	0.6351	0.6657	0.7203	0.7472
SO <sub>2</sub>	106.9	96.2	87.2	75.3	64.9	56.2	Annual	0.004	0.004	0.004	0.003	0.003	0.003
							24-Hour	0.06	0.06	0.06	0.06	0.06	0.05
							3-Hour	0.41	0.38	0.36	0.32	0.30	0.27
PM10	22.0	22.0	22.0	22.0	22.0	22.0	Annual	0.0008	0.0009	0.0009	0.0010	0.0011	0.0012
							24-Hour	0.013	0.013	0.016	0.017	0.019	0.020
NO <sub>x</sub>	352.1	316.9	287.3	248.2	213.9	185.2	Annual	0.013	0.012	0.012	0.011	0.011	0.010

(1) Concentrations are based on highest predicted concentrations using five years of meteorological for 1987 to 1991 of surface and upper air data from the National Weather Service stations at Tampa International Airport and Ruskin, respectively.

AIR PERMIT APPLICATION FOR  
DECKER ENERGY  
DECKER POWER PLANT  
FT. MEADE, FLORIDA

PREPARED BY  
GOLDER ASSOCIATES INC.  
6241 NW 23RD STREET, SUITE 500  
GAINESVILLE, FLORIDA 32653-1500  
(352) 336-5600

JUNE, 2000  
PROJECT NO. 993-9562-0700

BPIP / ISCST3 / CALPUFF AIR MODELING FILES  
FILE CONTENTS

### 1. BPIP MODEL

BPIP.ZIP - ZIPPED FILE CONTAINING THE FOLLOWING:

DECKBLDG.BPP	BPIP INPUT FILE FOR THE PROPOSED PROJECT
DECKBLDG.OUT	BPIP OUTPUT FILE - BUILDING DATA USED IN THE ISCST3 MODEL
DECKBLDG.SUM	BPIP OUTPUT FILE - DETAILED BUILDING ANALYSIS

### 2. ISCST3 MODEL (PROJECT IMPACTS ONLY)

#### *2.1 LOAD ANALYSES FOR DETERMINING WORST-CASE OPERATING LOAD NATURAL GAS AND FUEL OIL FIRING, CLASS I IMPACTS*

DEC1C1.ZIP - ZIPPED FILE FOR FUEL OIL FIRING CONTAINING THE FOLLOWING :

DEC1C1.I<YY>/O<YY>	ISCST INPUT/OUTPUT FILES FOR 5 YEARS FROM 1987 TO 1991 GENERIC MODEL RESULTS USING 10 G/S EMISSION RATE FOR 3 STACKS (YY= LAST 2 DIGITS OF YEAR)
--------------------	--

DEC1C1.SUM	SUMMARY OF MAXIMUM CONCENTRATIONS FROM THE ISCST3 MODEL FOR EACH YEAR
------------	--

DEC2C1.ZIP- ZIPPED FILE FOR NATURAL GAS FIRING CONTAINING THE FOLLOWING :

DEC2C1.I<YY>/O<YY>	ISCST INPUT/OUTPUT FILES FOR 5 YEARS FROM 1987 TO 1991 GENERIC MODEL RESULTS USING 10 G/S EMISSION RATE FOR 3 STACKS (YY= LAST 2 DIGITS OF YEAR)
--------------------	--

DEC2C1.SUM	SUMMARY OF MAXIMUM CONCENTRATIONS FROM THE ISCST3 MODEL FOR EACH YEAR
------------	--

#### *2.2 LOAD ANALYSES FOR DETERMINING WORST-CASE OPERATING LOAD NATURAL GAS AND FUEL OIL FIRING, CLASS II IMPACTS*

DEC1C2.ZIP- ZIPPED FILE FOR FUEL OIL FIRING CONTAINING THE FOLLOWING :

DEC1C2.I<YY>/O<YY> ISCST INPUT/OUTPUT FILES FOR 5 YEARS FROM 1987 TO 1991  
GENERIC MODEL RESULTS USING 10 G/S EMISSION RATE FOR 3  
STACKS (YY= LAST 2 DIGITS OF YEAR)

DEC1C2.SUM SUMMARY OF MAXIMUM CONCENTRATIONS FROM THE  
ISCST3 MODEL FOR EACH YEAR

DEC2C2.ZIP- ZIPPED FILE FOR NATURAL GAS FIRING CONTAINING THE FOLLOWING :

DEC2C2.I<YY>/O<YY> ISCST INPUT/OUTPUT FILES FOR 5 YEARS FROM 1987 TO 1991  
GENERIC MODEL RESULTS USING 10 G/S EMISSION RATE FOR 3  
STACKS (YY= LAST 2 DIGITS OF YEAR)

DEC2C2.SUM SUMMARY OF MAXIMUM CONCENTRATIONS FROM THE  
ISCST3 MODEL FOR EACH YEAR

### **2.3 REFINEMENTS FOR FUEL OIL CLASS II IMPACTS, USING SPECIFIC EMISSIONS AND PARAMETERS FOR SPECIFIC OPERATING LOAD.**

REFINE.ZIP - ZIPPED FILE FOR REFINEMENTS CONTAIN THE FOLLOWING:

RSANC2.I90/O90 1990, SO2 ANNUAL, INITIAL REFINEMENT

RRSANC2.I90/O90 1990, SO2 ANNUAL, FINAL REFINEMENT

RS24C2.I89/O89 1989, SO2 24-HOUR, INITIAL REFINEMENT

RRS24C2.I89/O89 1989, SO2 24-HOUR, FINAL REFINEMENT

RS03C2.I89/O89 1989, SO2 3-HOUR

RPANC2.I90/O90 1990, PM ANNUAL

RP24C2.I88/O88 1988, PM 24-HOUR

RNANC2.I90/O90 1990, NO2 ANNUAL, INITIAL REFINEMENT

RRNANC2.I90/O90 1990, NO2 ANNUAL, FINAL REFINEMENT

RC08C2.I88/O88 1988, CO ANNUAL

RC01C2.I87/O87 1987, CO ANNUAL

REFIN.SUM ISCST SUMMARY OF REFINEMENT FILES

### **3. CALPUFF MODEL (PROJECT IMPACTS ONLY)**

#### **3.1 CLASS I IMPACTS, FUEL OIL FIRING, FOR SO2, NO2, PM, SO4, NO3, CO**

ZIPPED FILES CONTAINING THE FOLLOWING:

PUFINP10.ZIP	CALPUFF INPUT FILES FOR 100 PERCENT LOAD
PUFINP50.ZIP	CALPUFF INPUT FILES FOR 50 PERCENT LOAD
PUFLST10.ZIP	CALPUFF LIST FILES FOR 100 PERCENT LOAD
PUFLST50.ZIP	CALPUFF LIST FILES FOR 50 PERCENT LOAD
PSTINP10.ZIP	CALPOST INPUT FILES (FOR SIG. ANALYSIS AND REGIONAL HAZE) FOR 100 PERCENT LOAD
PSTINP50.ZIP	CALPOST INPUT FILES (FOR SIG. ANALYSIS AND REGIONAL HAZE) FOR 50 PERCENT LOAD
PSTLST10.ZIP	CALPOST LIST FILES FOR 100 PERCENT LOAD
PSTLST50.ZIP	CALPOST LIST FILES FOR 50 PERCENT LOAD

ISCSOB3 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :DEC1C2.087  
 ISCST3 OUTPUT FILE NUMBER 2 :DEC1C2.088  
 ISCST3 OUTPUT FILE NUMBER 3 :DEC1C2.089  
 ISCST3 OUTPUT FILE NUMBER 4 :DEC1C2.090  
 ISCST3 OUTPUT FILE NUMBER 5 :DEC1C2.091

First title for last output file is: 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
 Second title for last output file is: FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
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SOURCE GROUP ID: BASE32

Annual

1987	0.01367	240.	15000.	87123124
1988	0.01314	220.	15000.	88123124
1989	0.01206	210.	300.	89123124
1990	0.01693	250.	15000.	90123124
1991	0.01509	240.	15000.	91123124

HIGH 24-Hour

1987	0.15597	80.	6500.	87040624
1988	0.21451	220.	15000.	88091324
1989	0.21465	180.	20000.	89012324
1990	0.20803	240.	15000.	90102724
1991	0.17011	270.	8500.	91061124

HIGH 8-Hour

1987	0.44012	60.	20000.	87120408
1988	0.41999	240.	20000.	88011524
1989	0.46713	180.	20000.	89012308
1990	0.42971	180.	20000.	90041208
1991	0.35574	240.	20000.	91122608

HIGH 3-Hour

1987	0.86013	110.	20000.	87031003
1988	0.81349	220.	20000.	88091324
1989	0.70018	350.	20000.	89060824
1990	1.00563	270.	1800.	90061315
1991	0.85391	70.	1800.	91051215

HIGH 1-Hour

1987	1.99984	20.	1600.	87070913
1988	1.76181	20.	1700.	88082914
1989	2.01896	130.	1600.	89083014
1990	1.94153	90.	1600.	90072414
1991	1.96708	330.	1600.	91052413

SOURCE GROUP ID: BASE95

Annual

1987	0.01451	240.	15000.	87123124
1988	0.01369	220.	15000.	88123124
1989	0.01212	200.	15000.	89123124
1990	0.01790	250.	12000.	90123124
1991	0.01604	240.	15000.	91123124

HIGH 24-Hour

1987	0.16052	250.	15000.	87112324
1988	0.22414	220.	15000.	88091324
1989	0.22401	180.	20000.	89012324
1990	0.21722	240.	15000.	90102724
1991	0.17464	270.	8500.	91061124

HIGH 8-Hour

1987	0.45999	60.	20000.	87120408
1988	0.43819	240.	20000.	88011524
1989	0.48859	180.	20000.	89012308
1990	0.44921	180.	20000.	90041208
1991	0.37377	240.	20000.	91122608

HIGH 3-Hour

1987	0.89647	110.	20000.	87031003
1988	0.84822	220.	20000.	88091324
1989	0.73043	350.	20000.	89060824
1990	1.01342	270.	1800.	90061315
1991	0.86472	70.	1800.	91051215

HIGH 1-Hour

1987	2.01446	20.	1600.	87070913
1988	2.02038	20.	1600.	88062313
1989	2.07703	330.	1600.	89032712
1990	2.07302	200.	1600.	90081313
1991	1.98192	330.	1600.	91052413

SOURCE GROUP ID: LD7532



Annual					
	1987	0.01623	240.	12000.	87123124
	1988	0.01530	220.	15000.	88123124
	1989	0.01364	200.	15000.	89123124
	1990	0.01994	250.	12000.	90123124
	1991	0.01800	240.	15000.	91123124
HIGH 24-Hour					
	1987	0.19633	240.	1800.	87072424
	1988	0.24542	220.	15000.	88091324
	1989	0.24952	180.	20000.	89012324
	1990	0.23793	240.	15000.	90102724
	1991	0.18592	270.	8500.	91061124
HIGH 8-Hour					
	1987	0.50323	60.	20000.	87120408
	1988	0.46174	240.	20000.	88011524
	1989	0.53518	180.	20000.	89012308
	1990	0.49153	180.	20000.	90041208
	1991	0.41350	240.	20000.	91122608
HIGH 3-Hour					
	1987	0.97500	110.	20000.	87031003
	1988	0.92421	220.	20000.	88091324
	1989	0.79684	350.	20000.	89060824
	1990	1.03082	270.	1800.	90061315
	1991	0.88796	70.	1800.	91051215
HIGH 1-Hour					
	1987	2.20804	110.	1600.	87080314
	1988	2.28390	70.	1600.	88080514
	1989	2.33798	250.	1600.	89080412
	1990	2.26697	70.	1600.	90090912
	1991	2.20383	320.	1600.	91061514
SOURCE GROUP ID: LD7592					
Annual					
	1987	0.01729	240.	15000.	87123124
	1988	0.01667	220.	15000.	88123124
	1989	0.01496	200.	15000.	89123124
	1990	0.02156	250.	12000.	90123124
	1991	0.01962	240.	15000.	91123124
HIGH 24-Hour					
	1987	0.20683	250.	12000.	87112324
	1988	0.26340	220.	15000.	88091324
	1989	0.26806	180.	15000.	89012324
	1990	0.25595	240.	15000.	90102724
	1991	0.19523	270.	8500.	91061124
HIGH 8-Hour					
	1987	0.54141	60.	15000.	87120408
	1988	0.53337	160.	1600.	88080716
	1989	0.57425	180.	20000.	89012308
	1990	0.52681	180.	20000.	90041208
	1991	0.44729	240.	20000.	91122608
HIGH 3-Hour					
	1987	1.04765	110.	15000.	87031003
	1988	0.98759	220.	20000.	88091324
	1989	0.85282	350.	15000.	89060824
	1990	1.21573	40.	1600.	90042312
	1991	0.91305	70.	1700.	91051215
HIGH 1-Hour					
	1987	2.50989	250.	1500.	87082212
	1988	2.53719	190.	1500.	88072912
	1989	2.42794	30.	1500.	89062011
	1990	2.47972	160.	1500.	90072613
	1991	2.43522	330.	1500.	91040612
SOURCE GROUP ID: LD5032					
Annual					
	1987	0.02006	250.	11000.	87123124
	1988	0.01890	220.	15000.	88123124
	1989	0.01746	180.	12000.	89123124
	1990	0.02530	250.	10000.	90123124
	1991	0.02261	240.	15000.	91123124
HIGH 24-Hour					
	1987	0.23496	250.	11000.	87112324
	1988	0.27288	220.	15000.	88091324
	1989	0.30493	180.	15000.	89012324
	1990	0.29083	240.	15000.	90102724
	1991	0.22854	250.	5250.	91090224
HIGH 8-Hour					
	1987	0.61818	60.	15000.	87120408
	1988	0.54654	160.	1600.	88080716

	1989	0.65539	180.	15000.	89012308
	1990	0.59683	180.	15000.	90041208
	1991	0.51093	240.	20000.	91122608
HIGH 3-Hour	1987	1.18722	110.	15000.	87031003
	1988	1.05975	220.	20000.	88091324
	1989	1.71136	330.	1500.	89062212
	1990	1.24117	40.	1600.	90042312
	1991	1.02702	270.	20000.	91010306
HIGH 1-Hour	1987	2.78019	100.	1500.	87090912
	1988	2.78302	60.	1500.	88092413
	1989	2.83612	330.	1500.	89062211
	1990	2.78516	310.	1500.	90090111
	1991	2.81295	50.	1500.	91081312
SOURCE GROUP ID:	LD5095				
Annual	1987	0.02160	250.	10000.	87123124
	1988	0.02008	220.	15000.	88123124
	1989	0.01891	180.	12000.	89123124
	1990	0.02751	250.	10000.	90123124
	1991	0.02425	240.	15000.	91123124
HIGH 24-Hour	1987	0.25539	270.	7500.	87052424
	1988	0.33219	160.	1600.	88080724
	1989	0.32488	180.	15000.	89012324
	1990	0.30969	240.	15000.	90102724
	1991	0.24001	250.	5000.	91090224
HIGH 8-Hour	1987	0.62341	60.	20000.	87120408
	1988	0.78896	160.	1600.	88080716
	1989	0.69908	180.	15000.	89012308
	1990	0.63582	180.	15000.	90041208
	1991	0.54467	240.	20000.	91122608
HIGH 3-Hour	1987	1.26000	110.	15000.	87031003
	1988	1.47108	170.	1500.	88080712
	1989	1.73579	330.	1500.	89062212
	1990	1.25441	40.	1600.	90042312
	1991	1.09171	270.	20000.	91010306
HIGH 1-Hour	1987	3.08048	110.	1400.	87061811
	1988	2.92821	170.	1500.	88080711
	1989	2.91525	20.	1500.	89071612
	1990	3.04789	340.	1400.	90051212
	1991	3.05486	50.	1400.	91042713

All receptor computations reported with respect to a user-specified origin  
 GRID 0.00 0.00  
 DISCRETE 0.00 0.00

CO STARTING  
 CO TITLEONE 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
 CO TITLETWO FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2  
 CO MODELOPT DFAULT CONC RURAL  
 CO AVERTIME PERIOD 24 8 3 1  
 CO POLLUTID GEN  
 CO DCAYCOEF .000000  
 CO RUNORNOT RUN  
 CO FINISHED

SO STARTING

\*\* Source Location Cards:  
 \*\* SRCID SRCTYP XS YS ZS  
 \*\* MODELING ORIGIN CT NO.2 STACK LOCATION  
 \*\* LOCATION IS USED FOR POLAR DISCRETE RECEPTORS.  
 \*\* CT STACK NUMBER CODE  
 \*\* -----  
 \*\* A - CT NO. 1  
 \*\* B - CT NO. 2  
 \*\* C - CT NO. 3

\*\* Source Location Cards:  
 \*\* SRCID SRCTYP XS YS ZS  
 \*\* UTM (m) (m) (m)  
 SO LOCATION BASE32A POINT -39.08 0.0 0.0  
 SO LOCATION BASE32B POINT 0.0 0.0 0.0  
 SO LOCATION BASE32C POINT 39.08 0.0 0.0  
 \*\*  
 SO LOCATION BASE95A POINT -39.08 0.0 0.0  
 SO LOCATION BASE95B POINT 0.0 0.0 0.0  
 SO LOCATION BASE95C POINT 39.08 0.0 0.0  
 \*\*  
 SO LOCATION LD7532A POINT -39.08 0.0 0.0  
 SO LOCATION LD7532B POINT 0.0 0.0 0.0  
 SO LOCATION LD7532C POINT 39.08 0.0 0.0  
 \*\*  
 SO LOCATION LD7595A POINT -39.08 0.0 0.0  
 SO LOCATION LD7595B POINT 0.0 0.0 0.0  
 SO LOCATION LD7595C POINT 39.08 0.0 0.0  
 \*\*  
 SO LOCATION LD5032A POINT -39.08 0.0 0.0  
 SO LOCATION LD5032B POINT 0.0 0.0 0.0  
 SO LOCATION LD5032C POINT 39.08 0.0 0.0  
 \*\*  
 SO LOCATION LD5095A POINT -39.08 0.0 0.0  
 SO LOCATION LD5095B POINT 0.0 0.0 0.0  
 SO LOCATION LD5095C POINT 39.08 0.0 0.0  
 \*\*

\*\* Source Parameter Cards:  
 \*\* POINT: SRCID QS HS TS VS DS  
 \*\* (g/s) (m) (K) (m/s) (m)  
 SO SRCPARAM BASE32A 3.334 18.3 852.0 37.1 6.4  
 SO SRCPARAM BASE32B 3.333 18.3 852.0 37.1 6.4  
 SO SRCPARAM BASE32C 3.333 18.3 852.0 37.1 6.4  
 \*\*  
 SO SRCPARAM BASE95A 3.334 18.3 884.0 34.7 6.4  
 SO SRCPARAM BASE95B 3.333 18.3 884.0 34.7 6.4  
 SO SRCPARAM BASE95C 3.333 18.3 884.0 34.7 6.4  
 \*\*  
 SO SRCPARAM LD7532A 3.334 18.3 913.0 30.9 6.4  
 SO SRCPARAM LD7532B 3.333 18.3 913.0 30.9 6.4  
 SO SRCPARAM LD7532C 3.333 18.3 913.0 30.9 6.4  
 \*\*  
 SO SRCPARAM LD7595A 3.334 18.3 922.0 28.4 6.4  
 SO SRCPARAM LD7595B 3.333 18.3 922.0 28.4 6.4  
 SO SRCPARAM LD7595C 3.333 18.3 922.0 28.4 6.4  
 \*\*  
 SO SRCPARAM LD5032A 3.334 18.3 864.0 25.5 6.4  
 SO SRCPARAM LD5032B 3.333 18.3 864.0 25.5 6.4  
 SO SRCPARAM LD5032C 3.333 18.3 864.0 25.5 6.4  
 \*\*  
 SO SRCPARAM LD5095A 3.334 18.3 851.0 24.0 6.4  
 SO SRCPARAM LD5095B 3.333 18.3 851.0 24.0 6.4  
 SO SRCPARAM LD5095C 3.333 18.3 851.0 24.0 6.4  
 \*\*

SO BUILDHGT BASE32A-BASE95A 14.33 14.33 14.33 14.33 14.63 14.63

SO	BUILDHGT	BASE32A-BASE95A	14.63	14.63	14.63	14.63	0.00	14.33
SO	BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	6.71	6.71
SO	BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	14.33	14.33
SO	BUILDHGT	BASE32A-BASE95A	0.00	0.00	0.00	0.00	14.33	14.33
SO	BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	6.71	6.71
SO	BUILDWID	BASE32A-BASE95A	12.74	14.10	15.03	15.50	24.40	23.57
SO	BUILDWID	BASE32A-BASE95A	23.32	23.54	23.80	23.33	0.00	15.03
SO	BUILDWID	BASE32A-BASE95A	15.50	15.50	15.03	14.10	11.18	9.10
SO	BUILDWID	BASE32A-BASE95A	12.74	14.10	15.03	15.50	15.50	15.03
SO	BUILDWID	BASE32A-BASE95A	0.00	0.00	0.00	0.00	14.10	15.03
SO	BUILDWID	BASE32A-BASE95A	15.50	15.50	15.03	14.10	11.18	9.10
**								
SO	BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	14.33	14.33
SO	BUILDHGT	BASE32B-BASE95B	14.33	0.00	0.00	0.00	0.00	14.33
SO	BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	6.71	6.71
SO	BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	14.33	14.33
SO	BUILDHGT	BASE32B-BASE95B	0.00	0.00	0.00	0.00	0.00	14.33
SO	BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	6.71	6.71
SO	BUILDWID	BASE32B-BASE95B	12.74	14.10	15.03	15.50	15.50	15.03
SO	BUILDWID	BASE32B-BASE95B	14.10	0.00	0.00	0.00	0.00	15.03
SO	BUILDWID	BASE32B-BASE95B	15.50	15.50	15.03	14.10	11.18	9.10
SO	BUILDWID	BASE32B-BASE95B	12.74	14.10	15.03	15.50	15.50	15.03
SO	BUILDWID	BASE32B-BASE95B	0.00	0.00	0.00	0.00	0.00	15.03
SO	BUILDWID	BASE32B-BASE95B	15.50	15.50	15.03	14.10	11.18	9.10
**								
SO	BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	14.33	14.33
SO	BUILDHGT	BASE32C-BASE95C	14.33	0.00	0.00	0.00	0.00	0.00
SO	BUILDHGT	BASE32C-BASE95C	0.00	6.71	6.71	6.71	6.71	6.71
SO	BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	14.33	14.33
SO	BUILDHGT	BASE32C-BASE95C	0.00	0.00	0.00	0.00	0.00	0.00
SO	BUILDHGT	BASE32C-BASE95C	0.00	6.71	6.71	6.71	6.71	6.71
SO	BUILDWID	BASE32C-BASE95C	12.74	14.10	15.03	15.50	15.50	15.03
SO	BUILDWID	BASE32C-BASE95C	14.10	0.00	0.00	0.00	0.00	0.00
SO	BUILDWID	BASE32C-BASE95C	0.00	15.28	14.37	13.02	11.28	9.20
SO	BUILDWID	BASE32C-BASE95C	12.74	14.10	15.03	15.50	15.50	15.03
SO	BUILDWID	BASE32C-BASE95C	0.00	0.00	0.00	0.00	0.00	0.00
SO	BUILDWID	BASE32C-BASE95C	0.00	15.28	14.37	13.02	11.28	9.20
**								
SO	BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	14.63	14.63
SO	BUILDHGT	LD7532A-LD7595A	14.63	14.63	14.63	14.63	0.00	14.33
SO	BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	6.71	6.71
SO	BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	14.33	14.33
SO	BUILDHGT	LD7532A-LD7595A	0.00	0.00	0.00	0.00	14.33	14.33
SO	BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	6.71	6.71
SO	BUILDWID	LD7532A-LD7595A	12.74	14.10	15.03	15.50	24.40	23.57
SO	BUILDWID	LD7532A-LD7595A	23.32	23.54	23.80	23.33	0.00	15.03
SO	BUILDWID	LD7532A-LD7595A	15.50	15.50	15.03	14.10	11.18	9.10
SO	BUILDWID	LD7532A-LD7595A	12.74	14.10	15.03	15.50	15.50	15.03
SO	BUILDWID	LD7532A-LD7595A	0.00	0.00	0.00	0.00	14.10	15.03
SO	BUILDWID	LD7532A-LD7595A	15.50	15.50	15.03	14.10	11.18	9.10
**								
SO	BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	14.33	14.33
SO	BUILDHGT	LD7532B-LD7595B	14.33	0.00	0.00	0.00	0.00	14.33
SO	BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	6.71	6.71
SO	BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	14.33	14.33
SO	BUILDHGT	LD7532B-LD7595B	0.00	0.00	0.00	0.00	0.00	14.33
SO	BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	6.71	6.71
SO	BUILDWID	LD7532B-LD7595B	12.74	14.10	15.03	15.50	15.50	15.03
SO	BUILDWID	LD7532B-LD7595B	14.10	0.00	0.00	0.00	0.00	15.03
SO	BUILDWID	LD7532B-LD7595B	15.50	15.50	15.03	14.10	11.18	9.10
SO	BUILDWID	LD7532B-LD7595B	12.74	14.10	15.03	15.50	15.50	15.03
SO	BUILDWID	LD7532B-LD7595B	0.00	0.00	0.00	0.00	0.00	15.03
SO	BUILDWID	LD7532B-LD7595B	15.50	15.50	15.03	14.10	11.18	9.10
**								
SO	BUILDHGT	LD7532C-LD7595C	14.33	14.33	14.33	14.33	14.33	14.33
SO	BUILDHGT	LD7532C-LD7595C	14.33	0.00	0.00	0.00	0.00	0.00
SO	BUILDHGT	LD7532C-LD7595C	0.00	6.71	6.71	6.71	6.71	6.71
SO	BUILDHGT	LD7532C-LD7595C	14.33	14.33	14.33	14.33	14.33	14.33
SO	BUILDHGT	LD7532C-LD7595C	0.00	0.00	0.00	0.00	0.00	0.00
SO	BUILDHGT	LD7532C-LD7595C	0.00	6.71	6.71	6.71	6.71	6.71
SO	BUILDWID	LD7532C-LD7595C	12.74	14.10	15.03	15.50	15.50	15.03
SO	BUILDWID	LD7532C-LD7595C	14.10	0.00	0.00	0.00	0.00	0.00
SO	BUILDWID	LD7532C-LD7595C	0.00	15.28	14.37	13.02	11.28	9.20
SO	BUILDWID	LD7532C-LD7595C	12.74	14.10	15.03	15.50	15.50	15.03
SO	BUILDWID	LD7532C-LD7595C	0.00	0.00	0.00	0.00	0.00	0.00
SO	BUILDWID	LD7532C-LD7595C	0.00	15.28	14.37	13.02	11.28	9.20
**								

SO BUILDHGT	LD5032A-LD5095A	14.33	14.33	14.33	14.33	14.63	14.63
SO BUILDHGT	LD5032A-LD5095A	14.63	14.63	14.63	14.63	0.00	14.33
SO BUILDHGT	LD5032A-LD5095A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032A-LD5095A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032A-LD5095A	0.00	0.00	0.00	0.00	14.33	14.33
SO BUILDHGT	LD5032A-LD5095A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	LD5032A-LD5095A	12.74	14.10	15.03	15.50	24.40	23.57
SO BUILDWID	LD5032A-LD5095A	23.32	23.54	23.80	23.33	0.00	15.03
SO BUILDWID	LD5032A-LD5095A	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	LD5032A-LD5095A	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032A-LD5095A	0.00	0.00	0.00	0.00	14.10	15.03
SO BUILDWID	LD5032A-LD5095A	15.50	15.50	15.03	14.10	11.18	9.10

\*\*

SO BUILDHGT	LD5032B-LD5095B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032B-LD5095B	14.33	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	LD5032B-LD5095B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032B-LD5095B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032B-LD5095B	0.00	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	LD5032B-LD5095B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	LD5032B-LD5095B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032B-LD5095B	14.10	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	LD5032B-LD5095B	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	LD5032B-LD5095B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032B-LD5095B	0.00	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	LD5032B-LD5095B	15.50	15.50	15.03	14.10	11.18	9.10

\*\*

SO BUILDHGT	LD5032C-LD5095C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032C-LD5095C	14.33	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032C-LD5095C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	LD5032C-LD5095C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032C-LD5095C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032C-LD5095C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032C-LD5095C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032C-LD5095C	14.10	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032C-LD5095C	0.00	15.28	14.37	13.02	11.28	9.20
SO BUILDWID	LD5032C-LD5095C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032C-LD5095C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032C-LD5095C	0.00	15.28	14.37	13.02	11.28	9.20

\*\*

SO EMISUNIT .100000E+07 (GRAMS/SEC) (MICROGRAMS/CUBIC-METER)

SO SRCGROUP	BASE32	BASE32A	BASE32B	BASE32C
SO SRCGROUP	BASE95	BASE95A	BASE95B	BASE95C
SO SRCGROUP	LD7532	LD7532A	LD7532B	LD7532C
SO SRCGROUP	LD7592	LD7595A	LD7595B	LD7595C
SO SRCGROUP	LD5032	LD5032A	LD5032B	LD5032C
SO SRCGROUP	LD5095	LD5095A	LD5095B	LD5095C

SO FINISHED

\*\*

RE STARTING

RE GRIDPOLR POL STA  
 RE GRIDPOLR POL ORIG 0.0 0.0  
 RE GRIDPOLR POL GDIR 36 10.00 10.00

RE GRIDPOLR POL DIST			300	400	500	600
RE GRIDPOLR POL DIST	700	800	900	1000	1100	1200
RE GRIDPOLR POL DIST	1300	1400	1500	1600	1700	1800
RE GRIDPOLR POL DIST	1900	2000	2100	2200	2300	2400
RE GRIDPOLR POL DIST	2500	2600	2700	2800	2900	3000
RE GRIDPOLR POL DIST	3250	3500	3750	4000	4250	4500
RE GRIDPOLR POL DIST	4750	5000	5250	5500	5750	6000
RE GRIDPOLR POL DIST	6500	7000	7500	8000	8500	9000
RE GRIDPOLR POL DIST	9500	10000	11000	12000	15000	20000

RE GRIDPOLR POL END

RE DISCPOLR	BASE32B	70.	10
RE DISCPOLR	BASE32B	100.	10
RE DISCPOLR	BASE32B	200.	10
RE DISCPOLR	BASE32B	74.	20
RE DISCPOLR	BASE32B	100.	20
RE DISCPOLR	BASE32B	200.	20
RE DISCPOLR	BASE32B	80.	30
RE DISCPOLR	BASE32B	100.	30
RE DISCPOLR	BASE32B	200.	30

RE DISCPOLR BASE32B	90.	40
RE DISCPOLR BASE32B	100.	40
RE DISCPOLR BASE32B	200.	40
RE DISCPOLR BASE32B	107.	50
RE DISCPOLR BASE32B	200.	50
RE DISCPOLR BASE32B	137.	60
RE DISCPOLR BASE32B	200.	60
RE DISCPOLR BASE32B	199.	70
RE DISCPOLR BASE32B	200.	70
RE DISCPOLR BASE32B	190.	80
RE DISCPOLR BASE32B	200.	80
RE DISCPOLR BASE32B	200.	90
RE DISCPOLR BASE32B	250.	90
RE DISCPOLR BASE32B	300.	90
RE DISCPOLR BASE32B	190.	100
RE DISCPOLR BASE32B	200.	100
RE DISCPOLR BASE32B	250.	100
RE DISCPOLR BASE32B	199.	110
RE DISCPOLR BASE32B	200.	110
RE DISCPOLR BASE32B	197.	120
RE DISCPOLR BASE32B	200.	120
RE DISCPOLR BASE32B	153.	130
RE DISCPOLR BASE32B	200.	130
RE DISCPOLR BASE32B	129.	140
RE DISCPOLR BASE32B	200.	140
RE DISCPOLR BASE32B	114.	150
RE DISCPOLR BASE32B	200.	150
RE DISCPOLR BASE32B	105.	160
RE DISCPOLR BASE32B	200.	160
RE DISCPOLR BASE32B	100.	170
RE DISCPOLR BASE32B	200.	170
RE DISCPOLR BASE32B	99.	180
RE DISCPOLR BASE32B	100.	180
RE DISCPOLR BASE32B	200.	180
RE DISCPOLR BASE32B	100.	190
RE DISCPOLR BASE32B	200.	190
RE DISCPOLR BASE32B	105.	200
RE DISCPOLR BASE32B	200.	200
RE DISCPOLR BASE32B	114.	210
RE DISCPOLR BASE32B	200.	210
RE DISCPOLR BASE32B	129.	220
RE DISCPOLR BASE32B	200.	220
RE DISCPOLR BASE32B	153.	230
RE DISCPOLR BASE32B	200.	230
RE DISCPOLR BASE32B	197.	240
RE DISCPOLR BASE32B	200.	240
RE DISCPOLR BASE32B	204.	250
RE DISCPOLR BASE32B	195.	260
RE DISCPOLR BASE32B	200.	260
RE DISCPOLR BASE32B	192.	270
RE DISCPOLR BASE32B	200.	270
RE DISCPOLR BASE32B	173.	280
RE DISCPOLR BASE32B	200.	280
RE DISCPOLR BASE32B	141.	290
RE DISCPOLR BASE32B	200.	290
RE DISCPOLR BASE32B	119.	300
RE DISCPOLR BASE32B	200.	300
RE DISCPOLR BASE32B	99.	310
RE DISCPOLR BASE32B	100.	310
RE DISCPOLR BASE32B	200.	310
RE DISCPOLR BASE32B	87.	320
RE DISCPOLR BASE32B	100.	320
RE DISCPOLR BASE32B	200.	320
RE DISCPOLR BASE32B	80.	330
RE DISCPOLR BASE32B	100.	330
RE DISCPOLR BASE32B	200.	330
RE DISCPOLR BASE32B	74.	340
RE DISCPOLR BASE32B	100.	340
RE DISCPOLR BASE32B	200.	340
RE DISCPOLR BASE32B	70.	350
RE DISCPOLR BASE32B	100.	350
RE DISCPOLR BASE32B	200.	350
RE DISCPOLR BASE32B	69.	360
RE DISCPOLR BASE32B	100.	360
RE DISCPOLR BASE32B	200.	360

RE FINISHED

\*\*  
 ME STARTING  
 ME INPUTFIL P:\MET\TPATPA87.MET  
 ME ANEMHGHT 22 FEET  
 ME SURFDATA 12842 1987 TAMPA  
 ME UAIRDATA 12842 1987 TAMPA  
 ME WINDCATS 1.54 3.09 5.14 8.23 10.80  
 ME FINISHED  
 \*\*

OU STARTING  
 OU RECTABLE ALLAVE FIRST  
 OU FINISHED

\*\*\*\*\*  
 \*\*\* SETUP Finishes Successfully \*\*\*  
 \*\*\*\*\*

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE      04/21/00      \*\*\*      04/2  
 \*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2      \*\*\*      15:59  
 \*\*MODELOPTs:      PAGE

CONC      RURAL    FLAT      DFAULT

\*\*\*      MODEL SETUP OPTIONS SUMMARY      \*\*\*

-----  
 \*\*Intermediate Terrain Processing is Selected

\*\*Model Is Setup For Calculation of Average CONCentration Values.

-- SCAVENGING/DEPOSITION LOGIC --  
 \*\*Model Uses NO DRY DEPLETION. DDPLETE = F  
 \*\*Model Uses NO WET DEPLETION. WDPLETE = F  
 \*\*NO WET SCAVENGING Data Provided.  
 \*\*NO GAS DRY DEPOSITION Data Provided.  
 \*\*Model Does NOT Use GRIDDED TERRAIN Data for Depletion Calculations  
 \*\*Model Uses RURAL Dispersion.

\*\*Model Uses Regulatory DEFAULT Options:  
 1. Final Plume Rise.  
 2. Stack-tip Downwash.  
 3. Buoyancy-induced Dispersion.  
 4. Use Calms Processing Routine.  
 5. Not Use Missing Data Processing Routine.  
 6. Default Wind Profile Exponents.  
 7. Default Vertical Potential Temperature Gradients.  
 8. "Upper Bound" Values for Supersquat Buildings.  
 9. No Exponential Decay for RURAL Mode

\*\*Model Assumes Receptors on FLAT Terrain.

\*\*Model Assumes No FLAGPOLE Receptor Heights.

\*\*Model Calculates 4 Short Term Average(s) of: 24-HR 8-HR 3-HR 1-HR  
 and Calculates PERIOD Averages

\*\*This Run Includes: 18 Source(s); 6 Source Group(s); and 1956 Receptor(s)

\*\*The Model Assumes A Pollutant Type of: GEN

\*\*Model Set To Continue RUNNING After the Setup Testing.

\*\*Output Options Selected:  
 Model Outputs Tables of PERIOD Averages by Receptor  
 Model Outputs Tables of Highest Short Term Values by Receptor (RECTABLE Keyword)

\*\*NOTE: The Following Flags May Appear Following CONC Values: c for Calm Hours  
 m for Missing Hours  
 b for Both Calm and Missing Hours

\*\*Misc. Inputs: Anem. Hgt. (m) = 6.71 ; Decay Coef. = 0.000 ; Rot. Angle = 0.0  
 Emission Units = (GRAMS/SEC) ; Emission Rate Unit Factor = 0.10000E+07  
 Output Units = (MICROGRAMS/CUBIC-METER)

\*\*Approximate Storage Requirements of Model = 1.9 MB of RAM.

\*\*Input Runstream File: DEC1C2.i87

\*\*Output Print File: DEC1C2.087
\*\*\* ISCST3 - VERSION 99155 \*\*\*
\*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2

\*\*\* 04/2
\*\*\* 15:59
\*\*\* PAGE

\*\*MODELOPTs:
CONC RURAL FLAT DFAULT

\*\*\* POINT SOURCE DATA \*\*\*

Table with columns: SOURCE ID, NUMBER PART. CATS., EMISSION RATE (USER UNITS), X (METERS), Y (METERS), BASE ELEV. (METERS), STACK HEIGHT (METERS), STACK TEMP. (DEG.K), STACK EXIT VEL. (M/SEC), STACK DIAMETER (METERS), BUILDING EXISTS, EMISSION RATE SCALAR VARY BY.

\*\*\* ISCST3 - VERSION 99155 \*\*\*
\*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2

\*\*\* 04/2
\*\*\* 15:59
\*\*\* PAGE

\*\*MODELOPTs:
CONC RURAL FLAT DFAULT

\*\*\* SOURCE IDs DEFINING SOURCE GROUPS \*\*\*

Table with columns: GROUP ID, SOURCE IDs. Lists groupings for BASE32, BASE95, LD7532, LD7592, LD5032, LD5095.

\*\*\* ISCST3 - VERSION 99155 \*\*\*
\*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2

\*\*\* 04/2
\*\*\* 15:59
\*\*\* PAGE

\*\*MODELOPTs:
CONC RURAL FLAT DFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

Table with columns: SOURCE ID: BASE32A, IFV, BH, BW, WAK. Lists dimensions for 24 different source IDs.



25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	14.3,	14.1,	0	30	14.3,	1
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	

SOURCE ID: BASE32B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH					
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	1
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	14.3,	1
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	1
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	14.3,	1
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	

SOURCE ID: BASE32C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH					
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	1
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	0.0,	
13	0.0,	0.0,	0	14	6.7,	15.3,	0	15	6.7,	14.4,	0	16	6.7,	13.0,	0	17	6.7,	11.3,	0	18	6.7,	
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	1
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	0.0,	
31	0.0,	0.0,	0	32	6.7,	15.3,	0	33	6.7,	14.4,	0	34	6.7,	13.0,	0	35	6.7,	11.3,	0	36	6.7,	

SOURCE ID: BASE95A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH					
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.6,	24.4,	0	6	14.6,	2
7	14.6,	23.3,	0	8	14.6,	23.5,	0	9	14.6,	23.8,	0	10	14.6,	23.3,	0	11	0.0,	0.0,	0	12	14.3,	1
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	1
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	14.3,	14.1,	0	30	14.3,	1
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	

\*\*\* ISCST3 - VERSION 99155 \*\*\*

\*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00

\*\*\*

04/2

\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2

\*\*\*

15:59

\*\*MODELOPTs:

CONC

RURAL

FLAT

DEFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: BASE95B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH					
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	1
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	14.3,	1
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	1
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	14.3,	1
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	

SOURCE ID: BASE95C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH					
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	1
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	0.0,	
13	0.0,	0.0,	0	14	6.7,	15.3,	0	15	6.7,	14.4,	0	16	6.7,	13.0,	0	17	6.7,	11.3,	0	18	6.7,	
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	1
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	0.0,	
31	0.0,	0.0,	0	32	6.7,	15.3,	0	33	6.7,	14.4,	0	34	6.7,	13.0,	0	35	6.7,	11.3,	0	36	6.7,	

SOURCE ID: LD7532A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH					
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.6,	24.4,	0	6	14.6,	2
7	14.6,	23.3,	0	8	14.6,	23.5,	0	9	14.6,	23.8,	0	10	14.6,	23.3,	0	11	0.0,	0.0,	0	12	14.3,	1
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	1
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	14.3,	14.1,	0	30	14.3,	1
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	

SOURCE ID: LD7532B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.3
7	14.3	14.1	0	8	0.0	0.0	0	9	0.0	0.0	0	10	0.0	0.0	0	11	0.0
13	14.3	15.5	0	14	14.3	15.5	0	15	14.3	15.0	0	16	14.3	14.1	0	17	6.7
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	0.0
31	14.3	15.5	0	32	14.3	15.5	0	33	14.3	15.0	0	34	14.3	14.1	0	35	6.7
																36	6.7

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE      04/21/00      \*\*\*      04/2

\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP.      CLASS 2      \*\*\*      15:59

\*\*MODELOPTs:  
CONC

RURAL      FLAT      DFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: LD7532C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.3
7	14.3	14.1	0	8	0.0	0.0	0	9	0.0	0.0	0	10	0.0	0.0	0	11	0.0
13	0.0	0.0	0	14	6.7	15.3	0	15	6.7	14.4	0	16	6.7	13.0	0	17	6.7
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	0.0
31	0.0	0.0	0	32	6.7	15.3	0	33	6.7	14.4	0	34	6.7	13.0	0	35	6.7
																36	6.7

SOURCE ID: LD7595A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.6
7	14.6	23.3	0	8	14.6	23.5	0	9	14.6	23.8	0	10	14.6	23.3	0	11	0.0
13	14.3	15.5	0	14	14.3	15.5	0	15	14.3	15.0	0	16	14.3	14.1	0	17	6.7
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	14.3
31	14.3	15.5	0	32	14.3	15.5	0	33	14.3	15.0	0	34	14.3	14.1	0	35	6.7
																36	6.7

SOURCE ID: LD7595B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.3
7	14.3	14.1	0	8	0.0	0.0	0	9	0.0	0.0	0	10	0.0	0.0	0	11	0.0
13	14.3	15.5	0	14	14.3	15.5	0	15	14.3	15.0	0	16	14.3	14.1	0	17	6.7
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	0.0
31	14.3	15.5	0	32	14.3	15.5	0	33	14.3	15.0	0	34	14.3	14.1	0	35	6.7
																36	6.7

SOURCE ID: LD7595C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.3
7	14.3	14.1	0	8	0.0	0.0	0	9	0.0	0.0	0	10	0.0	0.0	0	11	0.0
13	0.0	0.0	0	14	6.7	15.3	0	15	6.7	14.4	0	16	6.7	13.0	0	17	6.7
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	0.0
31	0.0	0.0	0	32	6.7	15.3	0	33	6.7	14.4	0	34	6.7	13.0	0	35	6.7
																36	6.7

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE      04/21/00      \*\*\*      04/2

\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP.      CLASS 2      \*\*\*      15:59

\*\*MODELOPTs:  
CONC

RURAL      FLAT      DFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: LD5032A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.6
7	14.6	23.3	0	8	14.6	23.5	0	9	14.6	23.8	0	10	14.6	23.3	0	11	0.0
13	14.3	15.5	0	14	14.3	15.5	0	15	14.3	15.0	0	16	14.3	14.1	0	17	6.7
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	14.3
																30	14.3

31 14.3, 15.5, 0 32 14.3, 15.5, 0 33 14.3, 15.0, 0 34 14.3, 14.1, 0 35 6.7, 11.2, 0 36 6.7,

SOURCE ID: LD5032B

Table with 18 columns (IFV, BH, BW, WAK) and 36 rows of numerical data for source LD5032B.

SOURCE ID: LD5032C

Table with 18 columns (IFV, BH, BW, WAK) and 36 rows of numerical data for source LD5032C.

SOURCE ID: LD5095A

Table with 18 columns (IFV, BH, BW, WAK) and 36 rows of numerical data for source LD5095A.

\*\*\* ISCST3 - VERSION 99155 \*\*\* \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00 \*\*\* 04/2
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2 \*\*\* 15:59 PAGE

\*\*MODELOPTs:
CONC

RURAL FLAT DFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: LD5095B

Table with 18 columns (IFV, BH, BW, WAK) and 36 rows of numerical data for source LD5095B.

SOURCE ID: LD5095C

Table with 18 columns (IFV, BH, BW, WAK) and 36 rows of numerical data for source LD5095C.

\*\*\* ISCST3 - VERSION 99155 \*\*\* \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00 \*\*\* 04/2
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2 \*\*\* 15:59 PAGE

\*\*MODELOPTs:
CONC

RURAL FLAT DFAULT

\*\*\* GRIDDED RECEPTOR NETWORK SUMMARY \*\*\*

\*\*\* NETWORK ID: POL ; NETWORK TYPE: GRIDPOLR \*\*\*

\*\*\* ORIGIN FOR POLAR NETWORK \*\*\*

X-ORIG = 0.00 ; Y-ORIG = 0.00 (METERS)

\*\*\* DISTANCE RANGES OF NETWORK \*\*\*  
(METERS)

300.0,	400.0,	500.0,	600.0,	700.0,	800.0,	900.0,	1000.0,	1100.0,	1200.0,
1300.0,	1400.0,	1500.0,	1600.0,	1700.0,	1800.0,	1900.0,	2000.0,	2100.0,	2200.0,
2300.0,	2400.0,	2500.0,	2600.0,	2700.0,	2800.0,	2900.0,	3000.0,	3250.0,	3500.0,
3750.0,	4000.0,	4250.0,	4500.0,	4750.0,	5000.0,	5250.0,	5500.0,	5750.0,	6000.0,
6500.0,	7000.0,	7500.0,	8000.0,	8500.0,	9000.0,	9500.0,	10000.0,	11000.0,	12000.0,
15000.0,	20000.0,								

\*\*\* DIRECTION RADIALS OF NETWORK \*\*\*  
(DEGREES)

10.0,	20.0,	30.0,	40.0,	50.0,	60.0,	70.0,	80.0,	90.0,	100.0,
110.0,	120.0,	130.0,	140.0,	150.0,	160.0,	170.0,	180.0,	190.0,	200.0,
210.0,	220.0,	230.0,	240.0,	250.0,	260.0,	270.0,	280.0,	290.0,	300.0,
310.0,	320.0,	330.0,	340.0,	350.0,	360.0,				

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE      04/21/00      \*\*\*      04/2  
 \*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP.      CLASS 2      \*\*\*      15:59  
 PAGE

\*\*MODELOPTs:  
 CONC                    RURAL   FLAT                    DFAULT

\*\*\* DISCRETE POLAR RECEPTORS \*\*\*  
 ORIGIN: (DIST, DIR, ZELEV, ZFLAG)  
 SRCID: (METERS,DEG,METERS,METERS)

BASE32B : (	70.0,	10.0,	0.0,	0.0);	BASE32B : (	100.0,	10.0,	0.0,	0.0);
BASE32B : (	200.0,	10.0,	0.0,	0.0);	BASE32B : (	74.0,	20.0,	0.0,	0.0);
BASE32B : (	100.0,	20.0,	0.0,	0.0);	BASE32B : (	200.0,	20.0,	0.0,	0.0);
BASE32B : (	80.0,	30.0,	0.0,	0.0);	BASE32B : (	100.0,	30.0,	0.0,	0.0);
BASE32B : (	200.0,	30.0,	0.0,	0.0);	BASE32B : (	90.0,	40.0,	0.0,	0.0);
BASE32B : (	100.0,	40.0,	0.0,	0.0);	BASE32B : (	200.0,	40.0,	0.0,	0.0);
BASE32B : (	107.0,	50.0,	0.0,	0.0);	BASE32B : (	200.0,	50.0,	0.0,	0.0);
BASE32B : (	137.0,	60.0,	0.0,	0.0);	BASE32B : (	200.0,	60.0,	0.0,	0.0);
BASE32B : (	199.0,	70.0,	0.0,	0.0);	BASE32B : (	200.0,	70.0,	0.0,	0.0);
BASE32B : (	190.0,	80.0,	0.0,	0.0);	BASE32B : (	200.0,	80.0,	0.0,	0.0);
BASE32B : (	200.0,	90.0,	0.0,	0.0);	BASE32B : (	250.0,	90.0,	0.0,	0.0);
BASE32B : (	300.0,	90.0,	0.0,	0.0);	BASE32B : (	190.0,	100.0,	0.0,	0.0);
BASE32B : (	200.0,	100.0,	0.0,	0.0);	BASE32B : (	250.0,	100.0,	0.0,	0.0);
BASE32B : (	199.0,	110.0,	0.0,	0.0);	BASE32B : (	200.0,	110.0,	0.0,	0.0);
BASE32B : (	197.0,	120.0,	0.0,	0.0);	BASE32B : (	200.0,	120.0,	0.0,	0.0);
BASE32B : (	153.0,	130.0,	0.0,	0.0);	BASE32B : (	200.0,	130.0,	0.0,	0.0);
BASE32B : (	129.0,	140.0,	0.0,	0.0);	BASE32B : (	200.0,	140.0,	0.0,	0.0);
BASE32B : (	114.0,	150.0,	0.0,	0.0);	BASE32B : (	200.0,	150.0,	0.0,	0.0);
BASE32B : (	105.0,	160.0,	0.0,	0.0);	BASE32B : (	200.0,	160.0,	0.0,	0.0);
BASE32B : (	100.0,	170.0,	0.0,	0.0);	BASE32B : (	200.0,	170.0,	0.0,	0.0);
BASE32B : (	99.0,	180.0,	0.0,	0.0);	BASE32B : (	100.0,	180.0,	0.0,	0.0);
BASE32B : (	200.0,	180.0,	0.0,	0.0);	BASE32B : (	100.0,	190.0,	0.0,	0.0);
BASE32B : (	200.0,	190.0,	0.0,	0.0);	BASE32B : (	105.0,	200.0,	0.0,	0.0);
BASE32B : (	200.0,	200.0,	0.0,	0.0);	BASE32B : (	114.0,	210.0,	0.0,	0.0);
BASE32B : (	200.0,	210.0,	0.0,	0.0);	BASE32B : (	129.0,	220.0,	0.0,	0.0);
BASE32B : (	200.0,	220.0,	0.0,	0.0);	BASE32B : (	153.0,	230.0,	0.0,	0.0);
BASE32B : (	200.0,	230.0,	0.0,	0.0);	BASE32B : (	197.0,	240.0,	0.0,	0.0);
BASE32B : (	200.0,	240.0,	0.0,	0.0);	BASE32B : (	204.0,	250.0,	0.0,	0.0);
BASE32B : (	195.0,	260.0,	0.0,	0.0);	BASE32B : (	200.0,	260.0,	0.0,	0.0);
BASE32B : (	192.0,	270.0,	0.0,	0.0);	BASE32B : (	200.0,	270.0,	0.0,	0.0);
BASE32B : (	173.0,	280.0,	0.0,	0.0);	BASE32B : (	200.0,	280.0,	0.0,	0.0);
BASE32B : (	141.0,	290.0,	0.0,	0.0);	BASE32B : (	200.0,	290.0,	0.0,	0.0);
BASE32B : (	119.0,	300.0,	0.0,	0.0);	BASE32B : (	200.0,	300.0,	0.0,	0.0);
BASE32B : (	99.0,	310.0,	0.0,	0.0);	BASE32B : (	100.0,	310.0,	0.0,	0.0);
BASE32B : (	200.0,	310.0,	0.0,	0.0);	BASE32B : (	87.0,	320.0,	0.0,	0.0);
BASE32B : (	100.0,	320.0,	0.0,	0.0);	BASE32B : (	200.0,	320.0,	0.0,	0.0);
BASE32B : (	80.0,	330.0,	0.0,	0.0);	BASE32B : (	100.0,	330.0,	0.0,	0.0);
BASE32B : (	200.0,	330.0,	0.0,	0.0);	BASE32B : (	74.0,	340.0,	0.0,	0.0);
BASE32B : (	100.0,	340.0,	0.0,	0.0);	BASE32B : (	200.0,	340.0,	0.0,	0.0);
BASE32B : (	70.0,	350.0,	0.0,	0.0);	BASE32B : (	100.0,	350.0,	0.0,	0.0);
BASE32B : (	200.0,	350.0,	0.0,	0.0);	BASE32B : (	69.0,	360.0,	0.0,	0.0);
BASE32B : (	100.0,	360.0,	0.0,	0.0);	BASE32B : (	200.0,	360.0,	0.0,	0.0);

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE      04/21/00      \*\*\*      04/2  
 \*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP.      CLASS 2      \*\*\*      15:59  
 PAGE

\*\*MODELOPTs:  
 CONC                    RURAL   FLAT                    DFAULT

\*\*\* METEOROLOGICAL DAYS SELECTED FOR PROCESSING \*\*\*



87	01	01	14	119.0	7.72	287.6	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	15	132.0	7.20	288.2	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	16	134.0	7.72	289.3	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	17	141.0	7.20	288.2	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	18	137.0	5.14	287.6	5	1286.4	1238.1	0.0000	0.0	0.0000	0	0.00
87	01	01	19	144.0	3.60	286.5	5	1281.2	1078.6	0.0000	0.0	0.0000	0	0.00
87	01	01	20	117.0	2.06	285.4	6	1276.0	919.0	0.0000	0.0	0.0000	0	0.00
87	01	01	21	110.0	1.54	284.8	7	1270.9	759.5	0.0000	0.0	0.0000	0	0.00
87	01	01	22	112.0	0.00	283.7	7	1265.7	600.0	0.0000	0.0	0.0000	0	0.00
87	01	01	23	120.0	2.57	283.7	6	1260.5	440.5	0.0000	0.0	0.0000	0	0.00
87	01	01	24	130.0	1.54	282.6	7	1255.4	281.0	0.0000	0.0	0.0000	0	0.00

\*\*\* NOTES: STABILITY CLASS 1=A, 2=B, 3=C, 4=D, 5=E AND 6=F.

FLOW VECTOR IS DIRECTION TOWARD WHICH WIND IS BLOWING.

\*\*\* ISCST3 - VERSION 99155 \*\*\* \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00 \*\*\*  
 \*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2 \*\*\*

\*\*\* 04/2  
 \*\*\* 15:59  
 PAGE

\*\*MODELOPTs:  
 CONC

RURAL FLAT DFAULT

\*\*\* THE 1ST HIGHEST 1-HR AVERAGE CONCENTRATION VALUES FOR SOURCE GROUP: LD5095 \*\*\*  
 INCLUDING SOURCE(S): LD5095A, LD5095B, LD5095C,

\*\*\* DISCRETE POLAR RECEPTOR POINTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

ORIGIN SRCID	DIST (M)	DIR (DEG)	CONC	(YYMMDDHH)	ORIGIN SRCID	DIST (M)	DIR (DEG)	CONC	(YYM)
BASE32B :	200.00	350.00	0.21703	(87122018)	BASE32B :	69.00	360.00	0.00614	(870)
BASE32B :	100.00	360.00	0.00080	(87121220)	BASE32B :	200.00	360.00	0.21549	(870)

\*\*\* ISCST3 - VERSION 99155 \*\*\* \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00 \*\*\*  
 \*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2 \*\*\*

\*\*\* 04/2  
 \*\*\* 15:59  
 PAGE

\*\*MODELOPTs:  
 CONC

RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF MAXIMUM PERIOD ( 8760 HRS) RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

GROUP ID	AVERAGE CONC	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWORK GRID-ID
BASE32	1ST HIGHEST VALUE IS	0.01367 AT ( -12990.38, -7500.00, 0.00, 0.00)	GP	POL
	2ND HIGHEST VALUE IS	0.01355 AT ( -10392.30, -6000.00, 0.00, 0.00)	GP	POL
	3RD HIGHEST VALUE IS	0.01345 AT ( -9526.28, -5500.00, 0.00, 0.00)	GP	POL
BASE95	1ST HIGHEST VALUE IS	0.01451 AT ( -12990.38, -7500.00, 0.00, 0.00)	GP	POL
	2ND HIGHEST VALUE IS	0.01443 AT ( -10392.30, -6000.00, 0.00, 0.00)	GP	POL
	3RD HIGHEST VALUE IS	0.01434 AT ( -9526.28, -5500.00, 0.00, 0.00)	GP	POL
LD7532	1ST HIGHEST VALUE IS	0.01623 AT ( -10392.30, -6000.00, 0.00, 0.00)	GP	POL
	2ND HIGHEST VALUE IS	0.01620 AT ( -12990.38, -7500.00, 0.00, 0.00)	GP	POL
	3RD HIGHEST VALUE IS	0.01618 AT ( -9526.28, -5500.00, 0.00, 0.00)	GP	POL
LD7592	1ST HIGHEST VALUE IS	0.01729 AT ( -12990.38, -7500.00, 0.00, 0.00)	GP	POL
	2ND HIGHEST VALUE IS	0.01728 AT ( -10392.30, -6000.00, 0.00, 0.00)	GP	POL
	3RD HIGHEST VALUE IS	0.01722 AT ( -9526.28, -5500.00, 0.00, 0.00)	GP	POL
LD5032	1ST HIGHEST VALUE IS	0.02006 AT ( -10336.62, -3762.22, 0.00, 0.00)	GP	POL
	2ND HIGHEST VALUE IS	0.02006 AT ( -9396.93, -3420.20, 0.00, 0.00)	GP	POL
	3RD HIGHEST VALUE IS	0.02002 AT ( -11276.31, -4104.24, 0.00, 0.00)	GP	POL
LD5095	1ST HIGHEST VALUE IS	0.02160 AT ( -9396.93, -3420.20, 0.00, 0.00)	GP	POL
	2ND HIGHEST VALUE IS	0.02158 AT ( -10336.62, -3762.22, 0.00, 0.00)	GP	POL
	3RD HIGHEST VALUE IS	0.02152 AT ( -8927.08, -3249.19, 0.00, 0.00)	GP	POL

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
 GP = GRIDPOLR  
 DC = DISCCART  
 DP = DISCPOLR  
 BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2

\*\*\* 04/2  
\*\*\* 15:59  
PAGE

\*\*MODELOPTs:

CONC RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF HIGHEST 24-HR RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

GROUP ID	AVERAGE CONC	DATE (YYMMDDHH)	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWO GRID-
BASE32 HIGH 1ST HIGH VALUE IS	0.15597c	ON 87040624: AT (	6401.25, 1128.71, 0.00, 0.00)	GP	POL
BASE95 HIGH 1ST HIGH VALUE IS	0.16052	ON 87112324: AT (	-14095.39, -5130.30, 0.00, 0.00)	GP	POL
LD7532 HIGH 1ST HIGH VALUE IS	0.19633c	ON 87072424: AT (	-1558.85, -900.00, 0.00, 0.00)	GP	POL
LD7592 HIGH 1ST HIGH VALUE IS	0.20683	ON 87112324: AT (	-11276.31, -4104.24, 0.00, 0.00)	GP	POL
LD5032 HIGH 1ST HIGH VALUE IS	0.23496	ON 87112324: AT (	-10336.62, -3762.22, 0.00, 0.00)	GP	POL
LD5095 HIGH 1ST HIGH VALUE IS	0.25539	ON 87052424: AT (	-7500.00, 0.00, 0.00, 0.00)	GP	POL

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
GP = GRIDPOLR  
DC = DISCCART  
DP = DISCPOLR  
BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2

\*\*\* 04/2  
\*\*\* 15:59  
PAGE

\*\*MODELOPTs:

CONC RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF HIGHEST 8-HR RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

GROUP ID	AVERAGE CONC	DATE (YYMMDDHH)	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWO GRID-
BASE32 HIGH 1ST HIGH VALUE IS	0.44012	ON 87120408: AT (	17320.51, 10000.00, 0.00, 0.00)	GP	POL
BASE95 HIGH 1ST HIGH VALUE IS	0.45999	ON 87120408: AT (	17320.51, 10000.00, 0.00, 0.00)	GP	POL
LD7532 HIGH 1ST HIGH VALUE IS	0.50323	ON 87120408: AT (	17320.51, 10000.00, 0.00, 0.00)	GP	POL
LD7592 HIGH 1ST HIGH VALUE IS	0.54141	ON 87120408: AT (	12990.38, 7500.00, 0.00, 0.00)	GP	POL
LD5032 HIGH 1ST HIGH VALUE IS	0.61818	ON 87120408: AT (	12990.38, 7500.00, 0.00, 0.00)	GP	POL
LD5095 HIGH 1ST HIGH VALUE IS	0.62341	ON 87120408: AT (	17320.51, 10000.00, 0.00, 0.00)	GP	POL

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
GP = GRIDPOLR  
DC = DISCCART  
DP = DISCPOLR  
BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2

\*\*\* 04/2  
\*\*\* 15:59  
PAGE

\*\*MODELOPTs:

CONC RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF HIGHEST 3-HR RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

GROUP ID	AVERAGE CONC	DATE (YYMMDDHH)	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWO GRID-
----------	--------------	-----------------	---------------------------------	---------	-------------

BASE32	HIGH	1ST HIGH VALUE IS	0.86013	ON 87031003: AT (	18793.85,	-6840.40,	0.00,	0.00)	GP	POL
BASE95	HIGH	1ST HIGH VALUE IS	0.89647	ON 87031003: AT (	18793.85,	-6840.40,	0.00,	0.00)	GP	POL
LD7532	HIGH	1ST HIGH VALUE IS	0.97500	ON 87031003: AT (	18793.85,	-6840.40,	0.00,	0.00)	GP	POL
LD7592	HIGH	1ST HIGH VALUE IS	1.04765	ON 87031003: AT (	14095.39,	-5130.30,	0.00,	0.00)	GP	POL
LD5032	HIGH	1ST HIGH VALUE IS	1.18722	ON 87031003: AT (	14095.39,	-5130.30,	0.00,	0.00)	GP	POL
LD5095	HIGH	1ST HIGH VALUE IS	1.26000	ON 87031003: AT (	14095.39,	-5130.30,	0.00,	0.00)	GP	POL

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
 GP = GRIDPOLR  
 DC = DISCCART  
 DP = DISCPOLR  
 BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE      04/21/00  
 \*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2

\*\*\* 04/2  
 \*\*\* 15:59  
 PAGE

\*\*MODELOPTs:  
 CONC                            RURAL   FLAT                    DFAULT

\*\*\* THE SUMMARY OF HIGHEST 1-HR RESULTS \*\*\*

\*\* CONC OF GEN                    IN (MICROGRAMS/CUBIC-METER)                    \*\*

GROUP ID	AVERAGE CONC	DATE (YYMMDDHH)	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWO GRID-
BASE32	HIGH 1ST HIGH VALUE IS	1.99984 ON 87070913: AT (	547.23, 1503.51, 0.00, 0.00)	GP	POL
BASE95	HIGH 1ST HIGH VALUE IS	2.01446 ON 87070913: AT (	547.23, 1503.51, 0.00, 0.00)	GP	POL
LD7532	HIGH 1ST HIGH VALUE IS	2.20804 ON 87080314: AT (	1503.51, -547.23, 0.00, 0.00)	GP	POL
LD7592	HIGH 1ST HIGH VALUE IS	2.50989 ON 87082212: AT (	-1409.54, -513.03, 0.00, 0.00)	GP	POL
LD5032	HIGH 1ST HIGH VALUE IS	2.78019 ON 87090912: AT (	1477.21, -260.47, 0.00, 0.00)	GP	POL
LD5095	HIGH 1ST HIGH VALUE IS	3.08048 ON 87061811: AT (	1315.57, -478.83, 0.00, 0.00)	GP	POL

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
 GP = GRIDPOLR  
 DC = DISCCART  
 DP = DISCPOLR  
 BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE      04/21/00  
 \*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 2

\*\*\* 04/2  
 \*\*\* 15:59  
 PAGE

\*\*MODELOPTs:  
 CONC                            RURAL   FLAT                    DFAULT

\*\*\* Message Summary : ISCST3 Model Execution \*\*\*

----- Summary of Total Messages -----

A Total of                    0 Fatal Error Message(s)  
 A Total of                    0 Warning Message(s)  
 A Total of                    531 Informational Message(s)  
 A Total of                    531 Calm Hours Identified

\*\*\*\*\* FATAL ERROR MESSAGES \*\*\*\*\*  
 \*\*\* NONE \*\*\*

\*\*\*\*\* WARNING MESSAGES \*\*\*\*\*  
 \*\*\* NONE \*\*\*

\*\*\*\*\*



\*\*\* ISCST3 Finishes Successfully \*\*\*  
\*\*\*\*\*



Annual					
	1987	0.01650	240.	12000.	87123124
	1988	0.01570	220.	15000.	88123124
	1989	0.01389	200.	15000.	89123124
	1990	0.02029	250.	12000.	90123124
	1991	0.01851	240.	15000.	91123124
HIGH 24-Hour					
	1987	0.19706	240.	1800.	87072424
	1988	0.24962	220.	15000.	88091324
	1989	0.25343	180.	20000.	89012324
	1990	0.24203	240.	15000.	90102724
	1991	0.18806	270.	8500.	91061124
HIGH 8-Hour					
	1987	0.51158	60.	20000.	87120408
	1988	0.46946	240.	20000.	88011524
	1989	0.54406	180.	20000.	89012308
	1990	0.49963	180.	20000.	90041208
	1991	0.42120	240.	20000.	91122608
HIGH 3-Hour					
	1987	0.99006	110.	20000.	87031003
	1988	0.93909	220.	20000.	88091324
	1989	0.80992	350.	20000.	89060824
	1990	1.03429	270.	1800.	90061315
	1991	0.89253	70.	1700.	91051215
HIGH 1-Hour					
	1987	2.21471	110.	1600.	87080314
	1988	2.35317	30.	1600.	88082213
	1989	2.34449	250.	1600.	89080412
	1990	2.29397	100.	1600.	90060812
	1991	2.37582	130.	1600.	91092113
SOURCE GROUP ID: LD7592					
Annual					
	1987	0.01765	240.	12000.	87123124
	1988	0.01701	220.	15000.	88123124
	1989	0.01524	200.	15000.	89123124
	1990	0.02209	250.	11000.	90123124
	1991	0.02022	240.	15000.	91123124
HIGH 24-Hour					
	1987	0.21060	250.	12000.	87112324
	1988	0.26806	220.	15000.	88091324
	1989	0.27300	180.	15000.	89012324
	1990	0.26063	240.	15000.	90102724
	1991	0.19771	270.	8500.	91061124
HIGH 8-Hour					
	1987	0.55187	60.	15000.	87120408
	1988	0.53511	160.	1600.	88080716
	1989	0.58446	180.	15000.	89012308
	1990	0.57125	160.	1600.	90061716
	1991	0.45593	240.	20000.	91122608
HIGH 3-Hour					
	1987	1.06678	110.	15000.	87031003
	1988	1.00580	220.	15000.	88091324
	1989	0.86923	350.	15000.	89060824
	1990	1.21918	40.	1600.	90042312
	1991	0.92022	270.	20000.	91010306
HIGH 1-Hour					
	1987	2.51721	250.	1500.	87082212
	1988	2.55331	360.	1500.	88081913
	1989	2.51546	180.	1500.	89041613
	1990	2.54619	20.	1500.	90050211
	1991	2.44167	330.	1500.	91040612
SOURCE GROUP ID: LD5032					
Annual					
	1987	0.02034	250.	11000.	87123124
	1988	0.01924	220.	15000.	88123124
	1989	0.01775	200.	15000.	89123124
	1990	0.02576	250.	10000.	90123124
	1991	0.02307	240.	15000.	91123124
HIGH 24-Hour					
	1987	0.24420	270.	7500.	87052424
	1988	0.27684	220.	15000.	88091324
	1989	0.30900	180.	15000.	89012324
	1990	0.29471	240.	15000.	90102724
	1991	0.23094	250.	5250.	91090224
HIGH 8-Hour					
	1987	0.62657	60.	15000.	87120408
	1988	0.54807	160.	1600.	88080716

	1989	0.66432	180.	15000.	89012308
	1990	0.60488	180.	15000.	90041208
	1991	0.51788	240.	20000.	91122608
HIGH 3-Hour	1987	1.20235	110.	15000.	87031003
	1988	1.07349	220.	20000.	88091324
	1989	1.71643	330.	1500.	89062212
	1990	1.24398	40.	1600.	90042312
	1991	1.04049	270.	20000.	91010306
HIGH 1-Hour	1987	2.87625	200.	1500.	87083012
	1988	2.78887	60.	1500.	88092413
	1989	2.84166	330.	1500.	89062211
	1990	2.79101	310.	1500.	90090111
	1991	2.81830	50.	1500.	91081312
SOURCE GROUP ID:	LD5095				
Annual	1987	0.02151	250.	10000.	87123124
	1988	0.02015	220.	15000.	88123124
	1989	0.01867	180.	12000.	89123124
	1990	0.02725	250.	10000.	90123124
	1991	0.02432	240.	15000.	91123124
HIGH 24-Hour	1987	0.25425	270.	7500.	87052424
	1988	0.33196	160.	1600.	88080724
	1989	0.32314	180.	15000.	89012324
	1990	0.30809	240.	15000.	90102724
	1991	0.23909	250.	5000.	91090224
HIGH 8-Hour	1987	0.62039	60.	20000.	87120408
	1988	0.78842	160.	1600.	88080716
	1989	0.69524	180.	15000.	89012308
	1990	0.63250	180.	15000.	90041208
	1991	0.54179	240.	20000.	91122608
HIGH 3-Hour	1987	1.25393	110.	15000.	87031003
	1988	1.47013	170.	1500.	88080712
	1989	1.73389	330.	1500.	89062212
	1990	1.25339	40.	1600.	90042312
	1991	1.08636	270.	20000.	91010306
HIGH 1-Hour	1987	3.07846	110.	1400.	87061811
	1988	2.92635	170.	1500.	88080711
	1989	2.91339	20.	1500.	89071612
	1990	2.98992	70.	1500.	90043014
	1991	3.05282	50.	1400.	91042713

All receptor computations reported with respect to a user-specified origin  
 GRID 0.00 0.00  
 DISCRETE 0.00 0.00

CO STARTING  
 CO TITLEONE 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
 CO TITLETWO NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1  
 CO MODELOPT DFAULT CONC RURAL  
 CO AVERTIME PERIOD 24 8 3 1  
 CO POLLUTID GEN  
 CO DCAYCOEF .000000  
 CO RUNORNOT RUN  
 CO FINISHED

SO STARTING

\*\* Source Location Cards:

\*\* SRCID SRCTYP XS YS ZS  
 \*\* MODELING ORIGIN CT NO.2 STACK LOCATION  
 \*\* CT STACK NUMBER CODE  
 \*\* -----  
 \*\* A - CT NO. 1  
 \*\* B - CT NO. 2  
 \*\* C - CT NO. 3

\*\* Source Location Cards:

SO	LOCATION	SRCID	SRCTYP	XS (m)	YS (m)	ZS (m)
**						
SO	LOCATION	BASE32A	POINT	419400	3069700	0.0
SO	LOCATION	BASE32B	POINT	419400	3069700	0.0
SO	LOCATION	BASE32C	POINT	419400	3069700	0.0
**						
SO	LOCATION	BASE95A	POINT	419400	3069700	0.0
SO	LOCATION	BASE95B	POINT	419400	3069700	0.0
SO	LOCATION	BASE95C	POINT	419400	3069700	0.0
**						
SO	LOCATION	LD7532A	POINT	419400	3069700	0.0
SO	LOCATION	LD7532B	POINT	419400	3069700	0.0
SO	LOCATION	LD7532C	POINT	419400	3069700	0.0
**						
SO	LOCATION	LD7595A	POINT	419400	3069700	0.0
SO	LOCATION	LD7595B	POINT	419400	3069700	0.0
SO	LOCATION	LD7595C	POINT	419400	3069700	0.0
**						
SO	LOCATION	LD5032A	POINT	419400	3069700	0.0
SO	LOCATION	LD5032B	POINT	419400	3069700	0.0
SO	LOCATION	LD5032C	POINT	419400	3069700	0.0
**						
SO	LOCATION	LD5095A	POINT	419400	3069700	0.0
SO	LOCATION	LD5095B	POINT	419400	3069700	0.0
SO	LOCATION	LD5095C	POINT	419400	3069700	0.0
**						

\*\* Source Parameter Cards:

SO	SRCPARAM	SRCID	QS (g/s)	HS (m)	TS (K)	VS (m/s)	DS (m)
**							
SO	SRCPARAM	BASE32A	3.334	18.3	853.0	36.2	6.4
SO	SRCPARAM	BASE32B	3.333	18.3	853.0	36.2	6.4
SO	SRCPARAM	BASE32C	3.333	18.3	853.0	36.2	6.4
**							
SO	SRCPARAM	BASE95A	3.334	18.3	880.0	33.6	6.4
SO	SRCPARAM	BASE95B	3.333	18.3	880.0	33.6	6.4
SO	SRCPARAM	BASE95C	3.333	18.3	880.0	33.6	6.4
**							
SO	SRCPARAM	LD7532A	3.334	18.3	902.0	30.5	6.4
SO	SRCPARAM	LD7532B	3.333	18.3	902.0	30.5	6.4
SO	SRCPARAM	LD7532C	3.333	18.3	902.0	30.5	6.4
**							
SO	SRCPARAM	LD7595A	3.334	18.3	911.0	28.0	6.4
SO	SRCPARAM	LD7595B	3.333	18.3	911.0	28.0	6.4
SO	SRCPARAM	LD7595C	3.333	18.3	911.0	28.0	6.4
**							
SO	SRCPARAM	LD5032A	3.334	18.3	853.0	25.3	6.4
SO	SRCPARAM	LD5032B	3.333	18.3	853.0	25.3	6.4
SO	SRCPARAM	LD5032C	3.333	18.3	853.0	25.3	6.4
**							
SO	SRCPARAM	LD5095A	3.334	18.3	840.0	24.3	6.4
SO	SRCPARAM	LD5095B	3.333	18.3	840.0	24.3	6.4
SO	SRCPARAM	LD5095C	3.333	18.3	840.0	24.3	6.4
**							
**							
SO	BUILDHGT	BASE32A-BASE95A		14.33	14.33	14.33	14.63
SO	BUILDHGT	BASE32A-BASE95A		14.63	14.63	14.63	0.00
							14.33

SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32A-BASE95A	0.00	0.00	0.00	0.00	14.33	14.33
SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	BASE32A-BASE95A	12.74	14.10	15.03	15.50	24.40	23.57
SO BUILDWID	BASE32A-BASE95A	23.32	23.54	23.80	23.33	0.00	15.03
SO BUILDWID	BASE32A-BASE95A	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	BASE32A-BASE95A	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32A-BASE95A	0.00	0.00	0.00	0.00	14.10	15.03
SO BUILDWID	BASE32A-BASE95A	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32B-BASE95B	14.33	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32B-BASE95B	0.00	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	BASE32B-BASE95B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32B-BASE95B	14.10	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	BASE32B-BASE95B	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	BASE32B-BASE95B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32B-BASE95B	0.00	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	BASE32B-BASE95B	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32C-BASE95C	14.33	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32C-BASE95C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32C-BASE95C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32C-BASE95C	14.10	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	15.28	14.37	13.02	11.28	9.20
SO BUILDWID	BASE32C-BASE95C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32C-BASE95C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	15.28	14.37	13.02	11.28	9.20
**							
SO BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	14.63	14.63
SO BUILDHGT	LD7532A-LD7595A	14.63	14.63	14.63	14.63	0.00	14.33
SO BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532A-LD7595A	0.00	0.00	0.00	0.00	14.33	14.33
SO BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	LD7532A-LD7595A	12.74	14.10	15.03	15.50	24.40	23.57
SO BUILDWID	LD7532A-LD7595A	23.32	23.54	23.80	23.33	0.00	15.03
SO BUILDWID	LD7532A-LD7595A	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	LD7532A-LD7595A	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532A-LD7595A	0.00	0.00	0.00	0.00	14.10	15.03
SO BUILDWID	LD7532A-LD7595A	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532B-LD7595B	14.33	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532B-LD7595B	0.00	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	LD7532B-LD7595B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532B-LD7595B	14.10	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	LD7532B-LD7595B	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	LD7532B-LD7595B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532B-LD7595B	0.00	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	LD7532B-LD7595B	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	LD7532C-LD7595C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532C-LD7595C	14.33	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD7532C-LD7595C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	LD7532C-LD7595C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532C-LD7595C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD7532C-LD7595C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD7532C-LD7595C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532C-LD7595C	14.10	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD7532C-LD7595C	0.00	15.28	14.37	13.02	11.28	9.20
SO BUILDWID	LD7532C-LD7595C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532C-LD7595C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD7532C-LD7595C	0.00	15.28	14.37	13.02	11.28	9.20
**							
SO BUILDHGT	LD5032A-LD5095A	14.33	14.33	14.33	14.33	14.63	14.63

SO BUILDHGT	LD5032A-LD5095A	14.63	14.63	14.63	14.63	0.00	14.33
SO BUILDHGT	LD5032A-LD5095A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032A-LD5095A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032A-LD5095A	0.00	0.00	0.00	0.00	14.33	14.33
SO BUILDHGT	LD5032A-LD5095A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	LD5032A-LD5095A	12.74	14.10	15.03	15.50	24.40	23.57
SO BUILDWID	LD5032A-LD5095A	23.32	23.54	23.80	23.33	0.00	15.03
SO BUILDWID	LD5032A-LD5095A	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	LD5032A-LD5095A	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032A-LD5095A	0.00	0.00	0.00	0.00	14.10	15.03
SO BUILDWID	LD5032A-LD5095A	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	LD5032B-LD5095B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032B-LD5095B	14.33	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	LD5032B-LD5095B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032B-LD5095B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032B-LD5095B	0.00	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	LD5032B-LD5095B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	LD5032B-LD5095B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032B-LD5095B	14.10	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	LD5032B-LD5095B	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	LD5032B-LD5095B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032B-LD5095B	0.00	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	LD5032B-LD5095B	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	LD5032C-LD5095C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032C-LD5095C	14.33	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032C-LD5095C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	LD5032C-LD5095C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032C-LD5095C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032C-LD5095C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032C-LD5095C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032C-LD5095C	14.10	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032C-LD5095C	0.00	15.28	14.37	13.02	11.28	9.20
SO BUILDWID	LD5032C-LD5095C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032C-LD5095C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032C-LD5095C	0.00	15.28	14.37	13.02	11.28	9.20

\*\*  
SO EMISUNIT .10000E+07 (GRAMS/SEC) (MICROGRAMS/CUBIC-METER)

SO SRCGROUP	BASE32	BASE32A	BASE32B	BASE32C
SO SRCGROUP	BASE95	BASE95A	BASE95B	BASE95C
SO SRCGROUP	LD7532	LD7532A	LD7532B	LD7532C
SO SRCGROUP	LD7595	LD7595A	LD7595B	LD7595C
SO SRCGROUP	LD5032	LD5032A	LD5032B	LD5032C
SO SRCGROUP	LD5095	LD5095A	LD5095B	LD5095C

SO FINISHED  
\*\*

RE STARTING  
\*\*

	UTM(m)	UTM(m)
RE DISCCART	340300	3165700
RE DISCCART	340300	3167700
RE DISCCART	340300	3169800
RE DISCCART	340700	3171900
RE DISCCART	342000	3174000
RE DISCCART	343000	3176200
RE DISCCART	343700	3178300
RE DISCCART	342400	3180600
RE DISCCART	341100	3183400
RE DISCCART	339000	3183400
RE DISCCART	336500	3183400
RE DISCCART	334000	3183400
RE DISCCART	331500	3183400

RE FINISHED  
\*\*

ME STARTING  
ME INPUTFIL P:\MET\TPATPA87.MET  
ME ANEMHGT 22 FEET  
ME SURFDATA 12842 1987 TAMPA  
ME UAIRDATA 12842 1987 TAMPA  
ME WINDCATS 1.54 3.09 5.14 8.23 10.80  
ME FINISHED  
\*\*

OU STARTING









\*\*\* ISCST3 - VERSION 99155 \*\*\*

\*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
\*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
\*\*\* 15:05:  
PAGE

\*\*MODELOPTS:  
CONC

RURAL FLAT DFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: LD7532C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.3	15
7	14.3	14.1	0	8	0.0	0.0	0	9	0.0	0.0	0	10	0.0	0.0	0	11	0.0	0
13	0.0	0.0	0	14	6.7	15.3	0	15	6.7	14.4	0	16	6.7	13.0	0	17	6.7	9
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3	15
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	0.0	0
31	0.0	0.0	0	32	6.7	15.3	0	33	6.7	14.4	0	34	6.7	13.0	0	35	6.7	9

SOURCE ID: LD7595A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.6	23
7	14.6	23.3	0	8	14.6	23.5	0	9	14.6	23.8	0	10	14.6	23.3	0	11	0.0	0
13	14.3	15.5	0	14	14.3	15.5	0	15	14.3	15.0	0	16	14.3	14.1	0	17	6.7	9
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3	15
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	14.3	15
31	14.3	15.5	0	32	14.3	15.5	0	33	14.3	15.0	0	34	14.3	14.1	0	35	6.7	9

SOURCE ID: LD7595B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.3	15
7	14.3	14.1	0	8	0.0	0.0	0	9	0.0	0.0	0	10	0.0	0.0	0	11	0.0	0
13	14.3	15.5	0	14	14.3	15.5	0	15	14.3	15.0	0	16	14.3	14.1	0	17	6.7	9
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3	15
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	0.0	0
31	14.3	15.5	0	32	14.3	15.5	0	33	14.3	15.0	0	34	14.3	14.1	0	35	6.7	9

SOURCE ID: LD7595C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.3	15
7	14.3	14.1	0	8	0.0	0.0	0	9	0.0	0.0	0	10	0.0	0.0	0	11	0.0	0
13	0.0	0.0	0	14	6.7	15.3	0	15	6.7	14.4	0	16	6.7	13.0	0	17	6.7	9
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3	15
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	0.0	0
31	0.0	0.0	0	32	6.7	15.3	0	33	6.7	14.4	0	34	6.7	13.0	0	35	6.7	9

\*\*\* ISCST3 - VERSION 99155 \*\*\*

\*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
\*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
\*\*\* 15:05:  
PAGE

\*\*MODELOPTS:  
CONC

RURAL FLAT DFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: LD5032A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.6	23
7	14.6	23.3	0	8	14.6	23.5	0	9	14.6	23.8	0	10	14.6	23.3	0	11	0.0	0
13	14.3	15.5	0	14	14.3	15.5	0	15	14.3	15.0	0	16	14.3	14.1	0	17	6.7	9
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3	15
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	14.3	15
31	14.3	15.5	0	32	14.3	15.5	0	33	14.3	15.0	0	34	14.3	14.1	0	35	6.7	9

SOURCE ID: LD5032B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.3	15
7	14.3	14.1	0	8	0.0	0.0	0	9	0.0	0.0	0	10	0.0	0.0	0	11	0.0	0
13	14.3	15.5	0	14	14.3	15.5	0	15	14.3	15.0	0	16	14.3	14.1	0	17	6.7	9
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3	15

25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9

SOURCE ID: LD5032C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	15
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	0.0,	0
13	0.0,	0.0,	0	14	6.7,	15.3,	0	15	6.7,	14.4,	0	16	6.7,	13.0,	0	17	6.7,	11.3,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	0.0,	0
31	0.0,	0.0,	0	32	6.7,	15.3,	0	33	6.7,	14.4,	0	34	6.7,	13.0,	0	35	6.7,	11.3,	0	36	6.7,	9

SOURCE ID: LD5095A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.6,	24.4,	0	6	14.6,	23
7	14.6,	23.3,	0	8	14.6,	23.5,	0	9	14.6,	23.8,	0	10	14.6,	23.3,	0	11	0.0,	0.0,	0	12	14.3,	15
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	14.3,	14.1,	0	30	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9

\*\*\* ICSCT3 - VERSION 99155 \*\*\*      \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00      \*\*\*      04/21  
 \*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1      \*\*\*      15:05:  
 \*\*MODELOPTs:      RURAL FLAT      DFAULT      \*\*\*      PAGE

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: LD5095B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	15
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	14.3,	15
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9

SOURCE ID: LD5095C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	15
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	0.0,	0
13	0.0,	0.0,	0	14	6.7,	15.3,	0	15	6.7,	14.4,	0	16	6.7,	13.0,	0	17	6.7,	11.3,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	0.0,	0
31	0.0,	0.0,	0	32	6.7,	15.3,	0	33	6.7,	14.4,	0	34	6.7,	13.0,	0	35	6.7,	11.3,	0	36	6.7,	9

\*\*\* ICSCT3 - VERSION 99155 \*\*\*      \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00      \*\*\*      04/21  
 \*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1      \*\*\*      15:05:  
 \*\*MODELOPTs:      RURAL FLAT      DFAULT      \*\*\*      PAGE

\*\*\* DISCRETE CARTESIAN RECEPTORS \*\*\*  
 (X-COORD, Y-COORD, ZELEV, ZFLAG)  
 (METERS)

( 340300.0, 3165700.0,	0.0,	0.0);	( 340300.0, 3167700.0,	0.0,	0.0);
( 340300.0, 3169800.0,	0.0,	0.0);	( 340700.0, 3171900.0,	0.0,	0.0);
( 342000.0, 3174000.0,	0.0,	0.0);	( 343000.0, 3176200.0,	0.0,	0.0);
( 343700.0, 3178300.0,	0.0,	0.0);	( 342400.0, 3180600.0,	0.0,	0.0);
( 341100.0, 3183400.0,	0.0,	0.0);	( 339000.0, 3183400.0,	0.0,	0.0);
( 336500.0, 3183400.0,	0.0,	0.0);	( 334000.0, 3183400.0,	0.0,	0.0);
( 331500.0, 3183400.0,	0.0,	0.0);			

\*\*\* ICSCT3 - VERSION 99155 \*\*\*      \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00      \*\*\*      04/21  
 \*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1      \*\*\*      15:05:  
 \*\*MODELOPTs:      RURAL FLAT      DFAULT      \*\*\*      PAGE



87	01	01	12	116.0	6.17	287.0	4	1182.0	1182.0	0.0000	0.0	0.0000	0	0.00
87	01	01	13	133.0	7.20	287.6	4	1235.0	1235.0	0.0000	0.0	0.0000	0	0.00
87	01	01	14	119.0	7.72	287.6	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	15	132.0	7.20	288.2	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	16	134.0	7.72	289.3	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	17	141.0	7.20	288.2	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	18	137.0	5.14	287.6	5	1286.4	1238.1	0.0000	0.0	0.0000	0	0.00
87	01	01	19	144.0	3.60	286.5	5	1281.2	1078.6	0.0000	0.0	0.0000	0	0.00
87	01	01	20	117.0	2.06	285.4	6	1276.0	919.0	0.0000	0.0	0.0000	0	0.00
87	01	01	21	110.0	1.54	284.8	7	1270.9	759.5	0.0000	0.0	0.0000	0	0.00
87	01	01	22	112.0	0.00	283.7	7	1265.7	600.0	0.0000	0.0	0.0000	0	0.00
87	01	01	23	120.0	2.57	283.7	6	1260.5	440.5	0.0000	0.0	0.0000	0	0.00
87	01	01	24	130.0	1.54	282.6	7	1255.4	281.0	0.0000	0.0	0.0000	0	0.00

\*\*\* NOTES: STABILITY CLASS 1=A, 2=B, 3=C, 4=D, 5=E AND 6=F.  
FLOW VECTOR IS DIRECTION TOWARD WHICH WIND IS BLOWING.

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
\*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
\*\*\* 15:05:  
PAGE

\*\*MODELOPTs:  
CONC

RURAL FLAT      DFAULT

\*\*\* THE SUMMARY OF MAXIMUM PERIOD ( 8760 HRS) RESULTS \*\*\*

GROUP ID		AVERAGE CONC	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWORK GRID-ID
BASE32	1ST HIGHEST VALUE IS	0.00215 AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
	2ND HIGHEST VALUE IS	0.00203 AT (	340300.00, 3167700.00,	0.00, 0.00)	DC NA
	3RD HIGHEST VALUE IS	0.00190 AT (	340300.00, 3169800.00,	0.00, 0.00)	DC NA
BASE95	1ST HIGHEST VALUE IS	0.00225 AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
	2ND HIGHEST VALUE IS	0.00211 AT (	340300.00, 3167700.00,	0.00, 0.00)	DC NA
	3RD HIGHEST VALUE IS	0.00198 AT (	340300.00, 3169800.00,	0.00, 0.00)	DC NA
LD7532	1ST HIGHEST VALUE IS	0.00240 AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
	2ND HIGHEST VALUE IS	0.00226 AT (	340300.00, 3167700.00,	0.00, 0.00)	DC NA
	3RD HIGHEST VALUE IS	0.00212 AT (	340300.00, 3169800.00,	0.00, 0.00)	DC NA
LD7595	1ST HIGHEST VALUE IS	0.00257 AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
	2ND HIGHEST VALUE IS	0.00241 AT (	340300.00, 3167700.00,	0.00, 0.00)	DC NA
	3RD HIGHEST VALUE IS	0.00226 AT (	340300.00, 3169800.00,	0.00, 0.00)	DC NA
LD5032	1ST HIGHEST VALUE IS	0.00283 AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
	2ND HIGHEST VALUE IS	0.00264 AT (	340300.00, 3167700.00,	0.00, 0.00)	DC NA
	3RD HIGHEST VALUE IS	0.00247 AT (	340300.00, 3169800.00,	0.00, 0.00)	DC NA
LD5095	1ST HIGHEST VALUE IS	0.00292 AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
	2ND HIGHEST VALUE IS	0.00272 AT (	340300.00, 3167700.00,	0.00, 0.00)	DC NA
	3RD HIGHEST VALUE IS	0.00254 AT (	340300.00, 3169800.00,	0.00, 0.00)	DC NA

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
GP = GRIDPOLR  
DC = DISCCART  
DP = DISCPOLR  
BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
\*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
\*\*\* 15:05:  
PAGE

\*\*MODELOPTs:  
CONC

RURAL FLAT      DFAULT

\*\*\* THE SUMMARY OF HIGHEST 24-HR RESULTS \*\*\*

GROUP ID		AVERAGE CONC	DATE (YYMMDDHH)	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWORK GRID-ID
BASE32	HIGH 1ST HIGH VALUE IS	0.03953c	ON 87122224:	AT ( 340300.00, 3165700.00,	0.00, 0.00)	DC NA

BASE95	HIGH	1ST HIGH VALUE IS	0.04061c	ON 87122224: AT (	340300.00,	3165700.00,	0.00,	0.00)	DC	NA
LD7532	HIGH	1ST HIGH VALUE IS	0.04216c	ON 87122224: AT (	340300.00,	3165700.00,	0.00,	0.00)	DC	NA
LD7595	HIGH	1ST HIGH VALUE IS	0.04363c	ON 87122224: AT (	340300.00,	3165700.00,	0.00,	0.00)	DC	NA
LD5032	HIGH	1ST HIGH VALUE IS	0.04616	ON 87061524: AT (	343000.00,	3176200.00,	0.00,	0.00)	DC	NA
LD5095	HIGH	1ST HIGH VALUE IS	0.04770	ON 87061524: AT (	343000.00,	3176200.00,	0.00,	0.00)	DC	NA

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
 GP = GRIDPOLR  
 DC = DISCCART  
 DP = DISCPOLR  
 BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\*  
 \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
 \*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
 \*\*\* 15:05:  
 \*\*\* PAGE

\*\*MODELOPTs:  
 CONC

RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF HIGHEST 8-HR RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

GROUP ID	AVERAGE CONC	DATE (YYMMDDHH)	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWORK GRID-I
BASE32	HIGH 1ST HIGH VALUE IS	0.14493c ON 87122208: AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
BASE95	HIGH 1ST HIGH VALUE IS	0.14889c ON 87122208: AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
LD7532	HIGH 1ST HIGH VALUE IS	0.15458c ON 87122208: AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
LD7595	HIGH 1ST HIGH VALUE IS	0.15997c ON 87122208: AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
LD5032	HIGH 1ST HIGH VALUE IS	0.16884c ON 87122208: AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
LD5095	HIGH 1ST HIGH VALUE IS	0.17200c ON 87122208: AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
 GP = GRIDPOLR  
 DC = DISCCART  
 DP = DISCPOLR  
 BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\*  
 \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
 \*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
 \*\*\* 15:05:  
 \*\*\* PAGE

\*\*MODELOPTs:  
 CONC

RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF HIGHEST 3-HR RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

GROUP ID	AVERAGE CONC	DATE (YYMMDDHH)	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWORK GRID-I
BASE32	HIGH 1ST HIGH VALUE IS	0.30919 ON 87011003: AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
BASE95	HIGH 1ST HIGH VALUE IS	0.31851 ON 87011003: AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
LD7532	HIGH 1ST HIGH VALUE IS	0.33197 ON 87011003: AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
LD7595	HIGH 1ST HIGH VALUE IS	0.34477 ON 87011003: AT (	340300.00, 3165700.00,	0.00, 0.00)	DC NA
LD5032	HIGH 1ST HIGH VALUE IS	0.36917 ON 87061506: AT (	343000.00, 3176200.00,	0.00, 0.00)	DC NA
LD5095	HIGH 1ST HIGH VALUE IS	0.38154 ON 87061506: AT (	343000.00, 3176200.00,	0.00, 0.00)	DC NA

\*\*\* RECEPTOR TYPES: GC = GRIDCART

GP = GRIDPOLR
DC = DISCCART
DP = DISCPOLR
BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\* \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00
\*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21
\*\*\* 15:05:
PAGE

\*\*MODELOPTs:
CONC RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF HIGHEST 1-HR RESULTS \*\*\*

Table with columns: GROUP ID, AVERAGE CONC, DATE (YYMMDDHH), RECEPTOR (XR, YR, ZELEV, ZFLAG), OF TYPE, NETWORK GRID-I. Rows include BASE32, BASE95, LD7532, LD7595, LD5032, LD5095.

\*\*\* RECEPTOR TYPES: GC = GRIDCART
GP = GRIDPOLR
DC = DISCCART
DP = DISCPOLR
BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\* \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00
\*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21
\*\*\* 15:05:
PAGE

\*\*MODELOPTs:
CONC RURAL FLAT DFAULT

\*\*\* Message Summary : ISCST3 Model Execution \*\*\*

----- Summary of Total Messages -----

A Total of 0 Fatal Error Message(s)
A Total of 0 Warning Message(s)
A Total of 531 Informational Message(s)
A Total of 531 Calm Hours Identified

\*\*\*\*\* FATAL ERROR MESSAGES \*\*\*\*\*
\*\*\* NONE \*\*\*

\*\*\*\*\* WARNING MESSAGES \*\*\*\*\*
\*\*\* NONE \*\*\*

\*\*\*\*\*
\*\*\* ISCST3 Finishes Successfully \*\*\*
\*\*\*\*\*



ISCB03 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :DEC1C1.087  
 ISCST3 OUTPUT FILE NUMBER 2 :DEC1C1.088  
 ISCST3 OUTPUT FILE NUMBER 3 :DEC1C1.089  
 ISCST3 OUTPUT FILE NUMBER 4 :DEC1C1.090  
 ISCST3 OUTPUT FILE NUMBER 5 :DEC1C1.091

First title for last output file is: 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
 Second title for last output file is: FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
-----					
SOURCE GROUP ID: BASE32					
Annual					
	1987	0.00211	340300.	3165700.	87123124
	1988	0.00302	340300.	3165700.	88123124
	1989	0.00301	343700.	3178300.	89123124
	1990	0.00196	340300.	3167700.	90123124
	1991	0.00204	340300.	3165700.	91123124
HIGH 24-Hour					
	1987	0.03909	340300.	3165700.	87122224
	1988	0.04699	343000.	3176200.	88112624
	1989	0.04564	340300.	3165700.	89100624
	1990	0.04335	341100.	3183400.	90021424
	1991	0.03423	340300.	3165700.	91072724
HIGH 8-Hour					
	1987	0.14331	340300.	3165700.	87122208
	1988	0.11439	343000.	3176200.	88082608
	1989	0.13647	340700.	3171900.	89093008
	1990	0.08447	341100.	3183400.	90021408
	1991	0.10256	343700.	3178300.	91072724
HIGH 3-Hour					
	1987	0.30540	340300.	3165700.	87011003
	1988	0.19833	343000.	3176200.	88060606
	1989	0.28330	340300.	3165700.	89030503
	1990	0.17332	340300.	3167700.	90112406
	1991	0.24682	342000.	3174000.	91120303
HIGH 1-Hour					
	1987	0.57952	340300.	3167700.	87072906
	1988	0.55801	340300.	3165700.	88092120
	1989	0.57855	340300.	3167700.	89091508
	1990	0.51997	340300.	3167700.	90112405
	1991	0.57827	340300.	3167700.	91070907
SOURCE GROUP ID: BASE95					
Annual					
	1987	0.00218	340300.	3165700.	87123124
	1988	0.00310	340300.	3165700.	88123124
	1989	0.00313	343700.	3178300.	89123124
	1990	0.00202	340300.	3167700.	90123124
	1991	0.00212	340300.	3165700.	91123124
HIGH 24-Hour					
	1987	0.03997	340300.	3165700.	87122224
	1988	0.04839	343000.	3176200.	88112624
	1989	0.04769	340300.	3165700.	89100624
	1990	0.04845	341100.	3183400.	90021424
	1991	0.03570	340300.	3165700.	91072724
HIGH 8-Hour					
	1987	0.14656	340300.	3165700.	87122208
	1988	0.11726	343000.	3176200.	88082608
	1989	0.13921	340700.	3171900.	89093008
	1990	0.08820	341100.	3183400.	90021408
	1991	0.10564	340300.	3165700.	91030608
HIGH 3-Hour					
	1987	0.31305	340300.	3165700.	87011003
	1988	0.20483	343000.	3176200.	88060606
	1989	0.29300	340300.	3165700.	89030503
	1990	0.17802	340300.	3167700.	90112406
	1991	0.25178	342000.	3174000.	91120303
HIGH 1-Hour					
	1987	0.59728	340300.	3167700.	87072906
	1988	0.57520	340300.	3165700.	88092120
	1989	0.59624	340300.	3167700.	89091508
	1990	0.53405	340300.	3167700.	90112405
	1991	0.59594	340300.	3167700.	91070907
SOURCE GROUP ID: LD7532					

Annual	1987	0.00238	340300.	3165700.	87123124
	1988	0.00333	340300.	3165700.	88123124
	1989	0.00341	343700.	3178300.	89123124
	1990	0.00219	340300.	3167700.	90123124
	1991	0.00227	340300.	3165700.	91123124
HIGH 24-Hour	1987	0.04181	340300.	3165700.	87122224
	1988	0.05141	343000.	3176200.	88112624
	1989	0.05663	340300.	3165700.	89100624
	1990	0.05162	341100.	3183400.	90021424
	1991	0.04180	340300.	3165700.	91072724
HIGH 8-Hour	1987	0.15331	340300.	3165700.	87122208
	1988	0.12332	343000.	3176200.	88082608
	1989	0.15224	340300.	3165700.	89100608
	1990	0.09630	341100.	3183400.	90021408
	1991	0.11328	340300.	3165700.	91030608
HIGH 3-Hour	1987	0.32900	340300.	3165700.	87011003
	1988	0.21886	343000.	3176200.	88060606
	1989	0.31384	340300.	3165700.	89030503
	1990	0.18785	340300.	3167700.	90112406
	1991	0.26234	340300.	3165700.	91052903
HIGH 1-Hour	1987	0.63512	340300.	3167700.	87072906
	1988	0.61183	340300.	3165700.	88092120
	1989	0.63401	340300.	3167700.	89091508
	1990	0.56355	340300.	3167700.	90112405
	1991	0.63369	340300.	3167700.	91070907
SOURCE GROUP ID:	LD7595				
Annual	1987	0.00254	340300.	3165700.	87123124
	1988	0.00355	340300.	3165700.	88123124
	1989	0.00366	343700.	3178300.	89123124
	1990	0.00230	340300.	3167700.	90123124
	1991	0.00241	340300.	3165700.	91123124
HIGH 24-Hour	1987	0.04327	340300.	3165700.	87122224
	1988	0.05384	343000.	3176200.	88112624
	1989	0.06059	340300.	3165700.	89100624
	1990	0.05424	341100.	3183400.	90021424
	1991	0.04444	340300.	3165700.	91072724
HIGH 8-Hour	1987	0.15865	340300.	3165700.	87122208
	1988	0.12815	343000.	3176200.	88082608
	1989	0.16362	340300.	3165700.	89100608
	1990	0.10303	341100.	3183400.	90021408
	1991	0.11956	340300.	3165700.	91030608
HIGH 3-Hour	1987	0.34165	340300.	3165700.	87011003
	1988	0.23040	343000.	3176200.	88060606
	1989	0.33091	340300.	3165700.	89030503
	1990	0.19570	340300.	3167700.	90112406
	1991	0.27517	340300.	3165700.	91052903
HIGH 1-Hour	1987	0.66569	340300.	3167700.	87072906
	1988	0.64144	340300.	3165700.	88092120
	1989	0.66455	340300.	3167700.	89091508
	1990	0.58709	340300.	3167700.	90112405
	1991	0.66422	340300.	3167700.	91070907
SOURCE GROUP ID:	LD5032				
Annual	1987	0.00279	340300.	3165700.	87123124
	1988	0.00391	340300.	3165700.	88123124
	1989	0.00408	343700.	3178300.	89123124
	1990	0.00248	340300.	3167700.	90123124
	1991	0.00266	340300.	3165700.	91123124
HIGH 24-Hour	1987	0.04579	340300.	3165700.	87122224
	1988	0.05892	340300.	3165700.	88073124
	1989	0.06770	340300.	3165700.	89100624
	1990	0.05900	341100.	3183400.	90021424
	1991	0.04958	340300.	3165700.	91072724
HIGH 8-Hour	1987	0.16788	340300.	3165700.	87122208
	1988	0.13665	343000.	3176200.	88082608

	1989	0.18494	340300.	3165700.	89100608
	1990	0.11541	341100.	3183400.	90021408
	1991	0.13088	340300.	3165700.	91030608
HIGH 3-Hour	1987	0.36548	343000.	3176200.	87061506
	1988	0.25141	343000.	3176200.	88060606
	1989	0.36185	340300.	3165700.	89030503
	1990	0.20940	340300.	3167700.	90112406
	1991	0.29839	340300.	3165700.	91052903
HIGH 1-Hour	1987	0.72027	340300.	3167700.	87072906
	1988	0.69432	340300.	3165700.	88092120
	1989	0.71922	340300.	3167700.	89091508
	1990	0.62821	340300.	3167700.	90112405
	1991	0.71892	340300.	3167700.	91070907
SOURCE GROUP ID:	LD5095				
Annual	1987	0.00292	340300.	3165700.	87123124
	1988	0.00406	340300.	3165700.	88123124
	1989	0.00424	343700.	3178300.	89123124
	1990	0.00257	340300.	3167700.	90123124
	1991	0.00278	340300.	3165700.	91123124
HIGH 24-Hour	1987	0.04787	343000.	3176200.	87061524
	1988	0.06182	340300.	3165700.	88073124
	1989	0.07138	340300.	3165700.	89100624
	1990	0.06143	341100.	3183400.	90021424
	1991	0.05230	340300.	3165700.	91072724
HIGH 8-Hour	1987	0.17236	340300.	3165700.	87122208
	1988	0.14078	343000.	3176200.	88082608
	1989	0.19598	340300.	3165700.	89100608
	1990	0.12179	341100.	3183400.	90021408
	1991	0.13665	340300.	3165700.	91030608
HIGH 3-Hour	1987	0.38290	343000.	3176200.	87061506
	1988	0.26204	343000.	3176200.	88060606
	1989	0.37744	340300.	3165700.	89030503
	1990	0.21613	340300.	3167700.	90112406
	1991	0.31001	340300.	3165700.	91052903
HIGH 1-Hour	1987	0.74720	340300.	3167700.	87072906
	1988	0.72042	340300.	3165700.	88092120
	1989	0.74618	340300.	3167700.	89091508
	1990	0.64838	340300.	3167700.	90112405
	1991	0.74588	340300.	3167700.	91070907

All receptor computations reported with respect to a user-specified origin  
 GRID 0.00 0.00  
 DISCRETE 0.00 0.00

CO STARTING  
 CO TITLEONE 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
 CO TITLETWO FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1  
 CO MODELOPT DFAULT CONC RURAL  
 CO AVERTIME PERIOD 24 8 3 1  
 CO POLLUTID GEN  
 CO DCAYCOEF .000000  
 CO RUNORNOT RUN  
 CO FINISHED

SO STARTING

\*\* Source Location Cards:

\*\* SRCID SRCTYP XS YS ZS  
 \*\* MODELING ORIGIN CT NO.2 STACK LOCATION  
 \*\* CT STACK NUMBER CODE

-----  
 \*\* A - CT NO. 1  
 \*\* B - CT NO. 2  
 \*\* C - CT NO. 3

\*\* Source Location Cards:

SRCID	SRCTYP	XS (m)	YS (m)	ZS (m)
SO LOCATION BASE32A POINT		419400	3069700	0.0
SO LOCATION BASE32B POINT		419400	3069700	0.0
SO LOCATION BASE32C POINT		419400	3069700	0.0
SO LOCATION BASE95A POINT		419400	3069700	0.0
SO LOCATION BASE95B POINT		419400	3069700	0.0
SO LOCATION BASE95C POINT		419400	3069700	0.0
SO LOCATION LD7532A POINT		419400	3069700	0.0
SO LOCATION LD7532B POINT		419400	3069700	0.0
SO LOCATION LD7532C POINT		419400	3069700	0.0
SO LOCATION LD7595A POINT		419400	3069700	0.0
SO LOCATION LD7595B POINT		419400	3069700	0.0
SO LOCATION LD7595C POINT		419400	3069700	0.0
SO LOCATION LD5032A POINT		419400	3069700	0.0
SO LOCATION LD5032B POINT		419400	3069700	0.0
SO LOCATION LD5032C POINT		419400	3069700	0.0
SO LOCATION LD5095A POINT		419400	3069700	0.0
SO LOCATION LD5095B POINT		419400	3069700	0.0
SO LOCATION LD5095C POINT		419400	3069700	0.0

\*\* Source Parameter Cards:

POINT: SRCID	QS (g/s)	HS (m)	TS (K)	VS (m/s)	DS (m)
SO SRCPARAM BASE32A	3.334	18.3	852.0	37.1	6.4
SO SRCPARAM BASE32B	3.333	18.3	852.0	37.1	6.4
SO SRCPARAM BASE32C	3.333	18.3	852.0	37.1	6.4
SO SRCPARAM BASE95A	3.334	18.3	884.0	34.7	6.4
SO SRCPARAM BASE95B	3.333	18.3	884.0	34.7	6.4
SO SRCPARAM BASE95C	3.333	18.3	884.0	34.7	6.4
SO SRCPARAM LD7532A	3.334	18.3	913.0	30.9	6.4
SO SRCPARAM LD7532B	3.333	18.3	913.0	30.9	6.4
SO SRCPARAM LD7532C	3.333	18.3	913.0	30.9	6.4
SO SRCPARAM LD7595A	3.334	18.3	922.0	28.4	6.4
SO SRCPARAM LD7595B	3.333	18.3	922.0	28.4	6.4
SO SRCPARAM LD7595C	3.333	18.3	922.0	28.4	6.4
SO SRCPARAM LD5032A	3.334	18.3	864.0	25.5	6.4
SO SRCPARAM LD5032B	3.333	18.3	864.0	25.5	6.4
SO SRCPARAM LD5032C	3.333	18.3	864.0	25.5	6.4
SO SRCPARAM LD5095A	3.334	18.3	851.0	24.0	6.4
SO SRCPARAM LD5095B	3.333	18.3	851.0	24.0	6.4
SO SRCPARAM LD5095C	3.333	18.3	851.0	24.0	6.4

SO BUILDHGT BASE32A-BASE95A 14.33 14.33 14.33 14.33 14.63 14.63  
 SO BUILDHGT BASE32A-BASE95A 14.63 14.63 14.63 14.63 0.00 14.33

SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32A-BASE95A	0.00	0.00	0.00	0.00	14.33	14.33
SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	BASE32A-BASE95A	12.74	14.10	15.03	15.50	24.40	23.57
SO BUILDWID	BASE32A-BASE95A	23.32	23.54	23.80	23.33	0.00	15.03
SO BUILDWID	BASE32A-BASE95A	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	BASE32A-BASE95A	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32A-BASE95A	0.00	0.00	0.00	0.00	14.10	15.03
SO BUILDWID	BASE32A-BASE95A	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32B-BASE95B	14.33	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32B-BASE95B	0.00	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	BASE32B-BASE95B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32B-BASE95B	14.10	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	BASE32B-BASE95B	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	BASE32B-BASE95B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32B-BASE95B	0.00	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	BASE32B-BASE95B	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32C-BASE95C	14.33	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32C-BASE95C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32C-BASE95C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32C-BASE95C	14.10	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	15.28	14.37	13.02	11.28	9.20
SO BUILDWID	BASE32C-BASE95C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32C-BASE95C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	15.28	14.37	13.02	11.28	9.20
**							
**							
SO BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	14.63	14.63
SO BUILDHGT	LD7532A-LD7595A	14.63	14.63	14.63	14.63	0.00	14.33
SO BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532A-LD7595A	0.00	0.00	0.00	0.00	14.33	14.33
SO BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	LD7532A-LD7595A	12.74	14.10	15.03	15.50	24.40	23.57
SO BUILDWID	LD7532A-LD7595A	23.32	23.54	23.80	23.33	0.00	15.03
SO BUILDWID	LD7532A-LD7595A	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	LD7532A-LD7595A	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532A-LD7595A	0.00	0.00	0.00	0.00	14.10	15.03
SO BUILDWID	LD7532A-LD7595A	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532B-LD7595B	14.33	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532B-LD7595B	0.00	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	LD7532B-LD7595B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532B-LD7595B	14.10	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	LD7532B-LD7595B	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	LD7532B-LD7595B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532B-LD7595B	0.00	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	LD7532B-LD7595B	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	LD7532C-LD7595C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532C-LD7595C	14.33	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD7532C-LD7595C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	LD7532C-LD7595C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532C-LD7595C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD7532C-LD7595C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD7532C-LD7595C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532C-LD7595C	14.10	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD7532C-LD7595C	0.00	15.28	14.37	13.02	11.28	9.20
SO BUILDWID	LD7532C-LD7595C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532C-LD7595C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD7532C-LD7595C	0.00	15.28	14.37	13.02	11.28	9.20
**							

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**
SO BUILDHGT LD5032A-LD5095A      14.33  14.33  14.33  14.33  14.63  14.63
SO BUILDHGT LD5032A-LD5095A      14.63  14.63  14.63  14.63   0.00  14.33
SO BUILDHGT LD5032A-LD5095A      14.33  14.33  14.33  14.33   6.71   6.71
SO BUILDHGT LD5032A-LD5095A      14.33  14.33  14.33  14.33  14.33  14.33
SO BUILDHGT LD5032A-LD5095A         0.00   0.00   0.00   0.00  14.33  14.33
SO BUILDHGT LD5032A-LD5095A      14.33  14.33  14.33  14.33   6.71   6.71
SO BUILDWID LD5032A-LD5095A      12.74  14.10  15.03  15.50  24.40  23.57
SO BUILDWID LD5032A-LD5095A      23.32  23.54  23.80  23.33   0.00  15.03
SO BUILDWID LD5032A-LD5095A      15.50  15.50  15.03  14.10  11.18   9.10
SO BUILDWID LD5032A-LD5095A      12.74  14.10  15.03  15.50  15.50  15.03
SO BUILDWID LD5032A-LD5095A         0.00   0.00   0.00   0.00  14.10  15.03
SO BUILDWID LD5032A-LD5095A      15.50  15.50  15.03  14.10  11.18   9.10

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**
SO BUILDHGT LD5032B-LD5095B      14.33  14.33  14.33  14.33  14.33  14.33
SO BUILDHGT LD5032B-LD5095B      14.33   0.00   0.00   0.00   0.00  14.33
SO BUILDHGT LD5032B-LD5095B      14.33  14.33  14.33  14.33   6.71   6.71
SO BUILDHGT LD5032B-LD5095B      14.33  14.33  14.33  14.33  14.33  14.33
SO BUILDHGT LD5032B-LD5095B         0.00   0.00   0.00   0.00   0.00  14.33
SO BUILDHGT LD5032B-LD5095B      14.33  14.33  14.33  14.33   6.71   6.71
SO BUILDWID LD5032B-LD5095B      12.74  14.10  15.03  15.50  15.50  15.03
SO BUILDWID LD5032B-LD5095B      14.10   0.00   0.00   0.00   0.00  15.03
SO BUILDWID LD5032B-LD5095B      15.50  15.50  15.03  14.10  11.18   9.10
SO BUILDWID LD5032B-LD5095B      12.74  14.10  15.03  15.50  15.50  15.03
SO BUILDWID LD5032B-LD5095B         0.00   0.00   0.00   0.00   0.00  15.03
SO BUILDWID LD5032B-LD5095B      15.50  15.50  15.03  14.10  11.18   9.10

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**
SO BUILDHGT LD5032C-LD5095C      14.33  14.33  14.33  14.33  14.33  14.33
SO BUILDHGT LD5032C-LD5095C      14.33   0.00   0.00   0.00   0.00   0.00
SO BUILDHGT LD5032C-LD5095C         0.00   6.71   6.71   6.71   6.71   6.71
SO BUILDHGT LD5032C-LD5095C      14.33  14.33  14.33  14.33  14.33  14.33
SO BUILDHGT LD5032C-LD5095C         0.00   0.00   0.00   0.00   0.00   0.00
SO BUILDHGT LD5032C-LD5095C         0.00   6.71   6.71   6.71   6.71   6.71
SO BUILDWID LD5032C-LD5095C      12.74  14.10  15.03  15.50  15.50  15.03
SO BUILDWID LD5032C-LD5095C      14.10   0.00   0.00   0.00   0.00   0.00
SO BUILDWID LD5032C-LD5095C         0.00  15.28  14.37  13.02  11.28   9.20
SO BUILDWID LD5032C-LD5095C      12.74  14.10  15.03  15.50  15.50  15.03
SO BUILDWID LD5032C-LD5095C         0.00   0.00   0.00   0.00   0.00   0.00
SO BUILDWID LD5032C-LD5095C         0.00  15.28  14.37  13.02  11.28   9.20

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**
SO EMISUNIT      .100000E+07 (GRAMS/SEC)      (MICROGRAMS/CUBIC-METER)

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SO SRCGROUP BASE32  BASE32A  BASE32B  BASE32C
SO SRCGROUP BASE95  BASE95A  BASE95B  BASE95C
SO SRCGROUP LD7532  LD7532A  LD7532B  LD7532C
SO SRCGROUP LD7595  LD7595A  LD7595B  LD7595C
SO SRCGROUP LD5032  LD5032A  LD5032B  LD5032C
SO SRCGROUP LD5095  LD5095A  LD5095B  LD5095C

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**
SO FINISHED
RE STARTING
**
RE DISCCART      UTM(m)      UTM(m)
RE DISCCART      340300      3165700
RE DISCCART      340300      3167700
RE DISCCART      340300      3169800
RE DISCCART      340700      3171900
RE DISCCART      342000      3174000
RE DISCCART      343000      3176200
RE DISCCART      343700      3178300
RE DISCCART      342400      3180600
RE DISCCART      341100      3183400
RE DISCCART      339000      3183400
RE DISCCART      336500      3183400
RE DISCCART      334000      3183400
RE DISCCART      331500      3183400

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RE FINISHED
**
ME STARTING
ME INPUTFIL P:\MET\TPATPA87.MET
ME ANEMHGT      22 FEET
ME SURFDATA      12842      1987      TAMPA
ME UAIRDATA      12842      1987      TAMPA
ME WINDCATS      1.54      3.09      5.14      8.23      10.80
ME FINISHED
**

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13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9

SOURCE ID: BASE32C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	15
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	0.0,	0
13	0.0,	0.0,	0	14	6.7,	15.3,	0	15	6.7,	14.4,	0	16	6.7,	13.0,	0	17	6.7,	11.3,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	0.0,	0
31	0.0,	0.0,	0	32	6.7,	15.3,	0	33	6.7,	14.4,	0	34	6.7,	13.0,	0	35	6.7,	11.3,	0	36	6.7,	9

SOURCE ID: BASE95A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.6,	24.4,	0	6	14.6,	23
7	14.6,	23.3,	0	8	14.6,	23.5,	0	9	14.6,	23.8,	0	10	14.6,	23.3,	0	11	0.0,	0.0,	0	12	14.3,	15
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	14.3,	14.1,	0	30	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9

\*\*\* ISCST3 - VERSION 99155 \*\*\*

\*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
\*\*\* 13:39:  
PAGE

\*\*MODELOPTS:  
CONC

RURAL FLAT DEFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: BASE95B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	15
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	14.3,	15
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9

SOURCE ID: BASE95C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	15
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	0.0,	0
13	0.0,	0.0,	0	14	6.7,	15.3,	0	15	6.7,	14.4,	0	16	6.7,	13.0,	0	17	6.7,	11.3,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	0.0,	0
31	0.0,	0.0,	0	32	6.7,	15.3,	0	33	6.7,	14.4,	0	34	6.7,	13.0,	0	35	6.7,	11.3,	0	36	6.7,	9

SOURCE ID: LD7532A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.6,	24.4,	0	6	14.6,	23
7	14.6,	23.3,	0	8	14.6,	23.5,	0	9	14.6,	23.8,	0	10	14.6,	23.3,	0	11	0.0,	0.0,	0	12	14.3,	15
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	14.3,	14.1,	0	30	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9

SOURCE ID: LD7532B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	15
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	14.3,	15
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9

\*\*\* ISCST3 - VERSION 99155 \*\*\* \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00 \*\*\*  
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1 \*\*\*

\*\*\* 04/21  
13:39:  
PAGE

\*\*MODELOPTs:  
CONC RURAL FLAT DFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: LD7532C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.3	15
7	14.3	14.1	0	8	0.0	0.0	0	9	0.0	0.0	0	10	0.0	0.0	0	11	0.0	0
13	0.0	0.0	0	14	6.7	15.3	0	15	6.7	14.4	0	16	6.7	13.0	0	17	6.7	9
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3	15
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	0.0	0
31	0.0	0.0	0	32	6.7	15.3	0	33	6.7	14.4	0	34	6.7	13.0	0	35	6.7	9

SOURCE ID: LD7595A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.6	23
7	14.6	23.3	0	8	14.6	23.5	0	9	14.6	23.8	0	10	14.6	23.3	0	11	0.0	15
13	14.3	15.5	0	14	14.3	15.5	0	15	14.3	15.0	0	16	14.3	14.1	0	17	6.7	9
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3	15
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	14.3	15
31	14.3	15.5	0	32	14.3	15.5	0	33	14.3	15.0	0	34	14.3	14.1	0	35	6.7	9

SOURCE ID: LD7595B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.3	15
7	14.3	14.1	0	8	0.0	0.0	0	9	0.0	0.0	0	10	0.0	0.0	0	11	0.0	15
13	14.3	15.5	0	14	14.3	15.5	0	15	14.3	15.0	0	16	14.3	14.1	0	17	6.7	9
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3	15
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	0.0	15
31	14.3	15.5	0	32	14.3	15.5	0	33	14.3	15.0	0	34	14.3	14.1	0	35	6.7	9

SOURCE ID: LD7595C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.3	15
7	14.3	14.1	0	8	0.0	0.0	0	9	0.0	0.0	0	10	0.0	0.0	0	11	0.0	0
13	0.0	0.0	0	14	6.7	15.3	0	15	6.7	14.4	0	16	6.7	13.0	0	17	6.7	9
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3	15
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	0.0	0
31	0.0	0.0	0	32	6.7	15.3	0	33	6.7	14.4	0	34	6.7	13.0	0	35	6.7	9

\*\*\* ISCST3 - VERSION 99155 \*\*\* \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00 \*\*\*  
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1 \*\*\*

\*\*\* 04/21  
13:39:  
PAGE

\*\*MODELOPTs:  
CONC RURAL FLAT DFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: LD5032A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.6	23
7	14.6	23.3	0	8	14.6	23.5	0	9	14.6	23.8	0	10	14.6	23.3	0	11	0.0	15
13	14.3	15.5	0	14	14.3	15.5	0	15	14.3	15.0	0	16	14.3	14.1	0	17	6.7	9
19	14.3	12.7	0	20	14.3	14.1	0	21	14.3	15.0	0	22	14.3	15.5	0	23	14.3	15
25	0.0	0.0	0	26	0.0	0.0	0	27	0.0	0.0	0	28	0.0	0.0	0	29	14.3	15
31	14.3	15.5	0	32	14.3	15.5	0	33	14.3	15.0	0	34	14.3	14.1	0	35	6.7	9

SOURCE ID: LD5032B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3	12.7	0	2	14.3	14.1	0	3	14.3	15.0	0	4	14.3	15.5	0	5	14.3	15
7	14.3	14.1	0	8	0.0	0.0	0	9	0.0	0.0	0	10	0.0	0.0	0	11	0.0	15
13	14.3	15.5	0	14	14.3	15.5	0	15	14.3	15.0	0	16	14.3	14.1	0	17	6.7	9

19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9

SOURCE ID: LD5032C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B				
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	15
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	0.0,	0
13	0.0,	0.0,	0	14	6.7,	15.3,	0	15	6.7,	14.4,	0	16	6.7,	13.0,	0	17	6.7,	11.3,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	0.0,	0
31	0.0,	0.0,	0	32	6.7,	15.3,	0	33	6.7,	14.4,	0	34	6.7,	13.0,	0	35	6.7,	11.3,	0	36	6.7,	9

SOURCE ID: LD5095A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B				
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.6,	24.4,	0	6	14.6,	23
7	14.6,	23.3,	0	8	14.6,	23.5,	0	9	14.6,	23.8,	0	10	14.6,	23.3,	0	11	0.0,	0.0,	0	12	14.3,	15
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	14.3,	14.1,	0	30	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00      \*\*\*      04/21  
 \*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1      \*\*\*      13:39:

\*\*MODELOPTs:  
CONC

RURAL FLAT      DFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: LD5095B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B				
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	15
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	14.3,	15
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00      \*\*\*      04/21  
 \*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1      \*\*\*      13:39:

\*\*MODELOPTs:  
CONC

RURAL FLAT      DFAULT

\*\*\* DISCRETE CARTESIAN RECEPTORS \*\*\*  
(X-COORD, Y-COORD, ZELEV, ZFLAG)  
(METERS)

( 340300.0, 3165700.0,	0.0,	0.0);	( 340300.0, 3167700.0,	0.0,	0.0);
( 340300.0, 3169800.0,	0.0,	0.0);	( 340700.0, 3171900.0,	0.0,	0.0);
( 342000.0, 3174000.0,	0.0,	0.0);	( 343000.0, 3176200.0,	0.0,	0.0);
( 343700.0, 3178300.0,	0.0,	0.0);	( 342400.0, 3180600.0,	0.0,	0.0);
( 341100.0, 3183400.0,	0.0,	0.0);	( 339000.0, 3183400.0,	0.0,	0.0);
( 336500.0, 3183400.0,	0.0,	0.0);	( 334000.0, 3183400.0,	0.0,	0.0);
( 331500.0, 3183400.0,	0.0,	0.0);			

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00      \*\*\*      04/21  
 \*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1      \*\*\*      13:39:

\*\*MODELOPTs:  
CONC

RURAL FLAT      DFAULT



87	01	01	11	114.0	6.69	287.6	4	1128.9	1128.9	0.0000	0.0	0.0000	0	0.00
87	01	01	12	116.0	6.17	287.0	4	1182.0	1182.0	0.0000	0.0	0.0000	0	0.00
87	01	01	13	133.0	7.20	287.6	4	1235.0	1235.0	0.0000	0.0	0.0000	0	0.00
87	01	01	14	119.0	7.72	287.6	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	15	132.0	7.20	288.2	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	16	134.0	7.72	289.3	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	17	141.0	7.20	288.2	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	18	137.0	5.14	287.6	5	1286.4	1238.1	0.0000	0.0	0.0000	0	0.00
87	01	01	19	144.0	3.60	286.5	5	1281.2	1078.6	0.0000	0.0	0.0000	0	0.00
87	01	01	20	117.0	2.06	285.4	6	1276.0	919.0	0.0000	0.0	0.0000	0	0.00
87	01	01	21	110.0	1.54	284.8	7	1270.9	759.5	0.0000	0.0	0.0000	0	0.00
87	01	01	22	112.0	0.00	283.7	7	1265.7	600.0	0.0000	0.0	0.0000	0	0.00
87	01	01	23	120.0	2.57	283.7	6	1260.5	440.5	0.0000	0.0	0.0000	0	0.00
87	01	01	24	130.0	1.54	282.6	7	1255.4	281.0	0.0000	0.0	0.0000	0	0.00

\*\*\* NOTES: STABILITY CLASS 1=A, 2=B, 3=C, 4=D, 5=E AND 6=F.  
FLOW VECTOR IS DIRECTION TOWARD WHICH WIND IS BLOWING.

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\*      04/21  
\*\*\*      13:39:  
PAGE

\*\*MODELOPTs:  
CONC

RURAL    FLAT                    DFAULT

\*\*\* THE SUMMARY OF MAXIMUM PERIOD ( 8760 HRS) RESULTS \*\*\*

\*\* CONC OF GEN                    IN (MICROGRAMS/CUBIC-METER)                    \*\*

GROUP ID	AVERAGE CONC	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWORK GRID-ID
BASE32	1ST HIGHEST VALUE IS	0.00211 AT ( 340300.00, 3165700.00,	0.00, 0.00) DC	NA
	2ND HIGHEST VALUE IS	0.00198 AT ( 340300.00, 3167700.00,	0.00, 0.00) DC	NA
	3RD HIGHEST VALUE IS	0.00186 AT ( 340300.00, 3169800.00,	0.00, 0.00) DC	NA
BASE95	1ST HIGHEST VALUE IS	0.00218 AT ( 340300.00, 3165700.00,	0.00, 0.00) DC	NA
	2ND HIGHEST VALUE IS	0.00205 AT ( 340300.00, 3167700.00,	0.00, 0.00) DC	NA
	3RD HIGHEST VALUE IS	0.00193 AT ( 340300.00, 3169800.00,	0.00, 0.00) DC	NA
LD7532	1ST HIGHEST VALUE IS	0.00238 AT ( 340300.00, 3165700.00,	0.00, 0.00) DC	NA
	2ND HIGHEST VALUE IS	0.00223 AT ( 340300.00, 3167700.00,	0.00, 0.00) DC	NA
	3RD HIGHEST VALUE IS	0.00209 AT ( 340300.00, 3169800.00,	0.00, 0.00) DC	NA
LD7595	1ST HIGHEST VALUE IS	0.00254 AT ( 340300.00, 3165700.00,	0.00, 0.00) DC	NA
	2ND HIGHEST VALUE IS	0.00238 AT ( 340300.00, 3167700.00,	0.00, 0.00) DC	NA
	3RD HIGHEST VALUE IS	0.00223 AT ( 340300.00, 3169800.00,	0.00, 0.00) DC	NA
LD5032	1ST HIGHEST VALUE IS	0.00279 AT ( 340300.00, 3165700.00,	0.00, 0.00) DC	NA
	2ND HIGHEST VALUE IS	0.00261 AT ( 340300.00, 3167700.00,	0.00, 0.00) DC	NA
	3RD HIGHEST VALUE IS	0.00244 AT ( 340300.00, 3169800.00,	0.00, 0.00) DC	NA
LD5095	1ST HIGHEST VALUE IS	0.00292 AT ( 340300.00, 3165700.00,	0.00, 0.00) DC	NA
	2ND HIGHEST VALUE IS	0.00273 AT ( 340300.00, 3167700.00,	0.00, 0.00) DC	NA
	3RD HIGHEST VALUE IS	0.00255 AT ( 340300.00, 3169800.00,	0.00, 0.00) DC	NA

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
GP = GRIDPOLR  
DC = DISCCART  
DP = DISCPOLR  
BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\*      04/21  
\*\*\*      13:39:  
PAGE

\*\*MODELOPTs:  
CONC

RURAL    FLAT                    DFAULT

\*\*\* THE SUMMARY OF HIGHEST 24-HR RESULTS \*\*\*

\*\* CONC OF GEN                    IN (MICROGRAMS/CUBIC-METER)                    \*\*

GROUP ID	AVERAGE CONC	DATE (YYMMDDHH)	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWORK GRID-ID
----------	--------------	-----------------	---------------------------------	---------	-----------------

BASE32	HIGH	1ST HIGH VALUE IS	0.03909c	ON 87122224: AT (	340300.00,	3165700.00,	0.00,	0.00)	DC	NA
BASE95	HIGH	1ST HIGH VALUE IS	0.03997c	ON 87122224: AT (	340300.00,	3165700.00,	0.00,	0.00)	DC	NA
LD7532	HIGH	1ST HIGH VALUE IS	0.04181c	ON 87122224: AT (	340300.00,	3165700.00,	0.00,	0.00)	DC	NA
LD7595	HIGH	1ST HIGH VALUE IS	0.04327c	ON 87122224: AT (	340300.00,	3165700.00,	0.00,	0.00)	DC	NA
LD5032	HIGH	1ST HIGH VALUE IS	0.04579c	ON 87122224: AT (	340300.00,	3165700.00,	0.00,	0.00)	DC	NA
LD5095	HIGH	1ST HIGH VALUE IS	0.04787	ON 87061524: AT (	343000.00,	3176200.00,	0.00,	0.00)	DC	NA

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
 GP = GRIDPOLR  
 DC = DISCCART  
 DP = DISCPOLR  
 BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\* \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
 \*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
 \*\*\* 13:39:  
 PAGE

\*\*MODELOPTs:  
 CONC RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF HIGHEST 8-HR RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

GROUP ID	AVERAGE CONC	DATE (YYMMDDHH)	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWORK GRID-I
BASE32 HIGH 1ST HIGH VALUE IS	0.14331c	ON 87122208: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
BASE95 HIGH 1ST HIGH VALUE IS	0.14656c	ON 87122208: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD7532 HIGH 1ST HIGH VALUE IS	0.15331c	ON 87122208: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD7595 HIGH 1ST HIGH VALUE IS	0.15865c	ON 87122208: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD5032 HIGH 1ST HIGH VALUE IS	0.16788c	ON 87122208: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD5095 HIGH 1ST HIGH VALUE IS	0.17236c	ON 87122208: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
 GP = GRIDPOLR  
 DC = DISCCART  
 DP = DISCPOLR  
 BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\* \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
 \*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
 \*\*\* 13:39:  
 PAGE

\*\*MODELOPTs:  
 CONC RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF HIGHEST 3-HR RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

GROUP ID	AVERAGE CONC	DATE (YYMMDDHH)	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWORK GRID-I
BASE32 HIGH 1ST HIGH VALUE IS	0.30540	ON 87011003: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
BASE95 HIGH 1ST HIGH VALUE IS	0.31305	ON 87011003: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD7532 HIGH 1ST HIGH VALUE IS	0.32900	ON 87011003: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD7595 HIGH 1ST HIGH VALUE IS	0.34165	ON 87011003: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD5032 HIGH 1ST HIGH VALUE IS	0.36548	ON 87061506: AT (	343000.00, 3176200.00, 0.00, 0.00)	DC	NA
LD5095 HIGH 1ST HIGH VALUE IS	0.38290	ON 87061506: AT (	343000.00, 3176200.00, 0.00, 0.00)	DC	NA

\*\*\* RECEPTOR TYPES: GC = GRIDCART
GP = GRIDPOLR
DC = DISCCART
DP = DISCPOLR
BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21
\*\*\* 13:39:
PAGE

\*\*MODELOPTs:
CONC

RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF HIGHEST 1-HR RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

Table with columns: GROUP ID, AVERAGE CONC, DATE (YYMMDDHH), RECEPTOR (XR, YR, ZELEV, ZFLAG), OF TYPE, NETWORK GRID-I. Rows include BASE32, BASE95, LD7532, LD7595, LD5032, LD5095.

\*\*\* RECEPTOR TYPES: GC = GRIDCART
GP = GRIDPOLR
DC = DISCCART
DP = DISCPOLR
BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\* 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00
\*\*\* FUEL OIL, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21
\*\*\* 13:39:
PAGE

\*\*MODELOPTs:
CONC

RURAL FLAT DFAULT

\*\*\* Message Summary : ISCST3 Model Execution \*\*\*

----- Summary of Total Messages -----

A Total of 0 Fatal Error Message(s)
A Total of 0 Warning Message(s)
A Total of 531 Informational Message(s)
A Total of 531 Calm Hours Identified

\*\*\*\*\* FATAL ERROR MESSAGES \*\*\*\*\*
\*\*\* NONE \*\*\*

\*\*\*\*\* WARNING MESSAGES \*\*\*\*\*
\*\*\* NONE \*\*\*

\*\*\*\*\*
\*\*\* ISCST3 Finishes Successfully \*\*\*
\*\*\*\*\*

## ISCB03 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :DEC2C1.087  
 ISCST3 OUTPUT FILE NUMBER 2 :DEC2C1.088  
 ISCST3 OUTPUT FILE NUMBER 3 :DEC2C1.089  
 ISCST3 OUTPUT FILE NUMBER 4 :DEC2C1.090  
 ISCST3 OUTPUT FILE NUMBER 5 :DEC2C1.091

First title for last output file is: 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
 Second title for last output file is: NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

AVERAGING TIME	YEAR	CONC (ug/m <sup>3</sup> )	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
-----					
SOURCE GROUP ID: BASE32					
Annual					
	1987	0.00215	340300.	3165700.	87123124
	1988	0.00306	340300.	3165700.	88123124
	1989	0.00306	343700.	3178300.	89123124
	1990	0.00199	340300.	3167700.	90123124
	1991	0.00208	340300.	3165700.	91123124
HIGH 24-Hour					
	1987	0.03953	340300.	3165700.	87122224
	1988	0.04769	343000.	3176200.	88112624
	1989	0.04666	340300.	3165700.	89100624
	1990	0.04770	341100.	3183400.	90021424
	1991	0.03496	340300.	3165700.	91072724
HIGH 8-Hour					
	1987	0.14493	340300.	3165700.	87122208
	1988	0.11584	343000.	3176200.	88082608
	1989	0.13785	340700.	3171900.	89093008
	1990	0.08631	341100.	3183400.	90021408
	1991	0.10382	340300.	3165700.	91030608
HIGH 3-Hour					
	1987	0.30919	340300.	3165700.	87011003
	1988	0.20157	343000.	3176200.	88060606
	1989	0.28813	340300.	3165700.	89030503
	1990	0.17565	340300.	3167700.	90112406
	1991	0.24930	342000.	3174000.	91120303
HIGH 1-Hour					
	1987	0.58844	340300.	3167700.	87072906
	1988	0.56665	340300.	3165700.	88092120
	1989	0.58747	340300.	3167700.	89091508
	1990	0.52696	340300.	3167700.	90112405
	1991	0.58719	340300.	3167700.	91070907
SOURCE GROUP ID: BASE95					
Annual					
	1987	0.00225	340300.	3165700.	87123124
	1988	0.00318	340300.	3165700.	88123124
	1989	0.00322	343700.	3178300.	89123124
	1990	0.00209	340300.	3167700.	90123124
	1991	0.00216	340300.	3165700.	91123124
HIGH 24-Hour					
	1987	0.04061	340300.	3165700.	87122224
	1988	0.04942	343000.	3176200.	88112624
	1989	0.04921	340300.	3165700.	89100624
	1990	0.04952	341100.	3183400.	90021424
	1991	0.03679	340300.	3165700.	91072724
HIGH 8-Hour					
	1987	0.14889	340300.	3165700.	87122208
	1988	0.11935	343000.	3176200.	88082608
	1989	0.14329	340300.	3165700.	89100608
	1990	0.09092	341100.	3183400.	90021408
	1991	0.10821	340300.	3165700.	91030608
HIGH 3-Hour					
	1987	0.31851	340300.	3165700.	87011003
	1988	0.20961	343000.	3176200.	88060606
	1989	0.30009	340300.	3165700.	89030503
	1990	0.18138	340300.	3167700.	90112406
	1991	0.25534	342000.	3174000.	91120303
HIGH 1-Hour					
	1987	0.61029	340300.	3167700.	87072906
	1988	0.58779	340300.	3165700.	88092120
	1989	0.60925	340300.	3167700.	89091508
	1990	0.54415	340300.	3167700.	90112405
	1991	0.60895	340300.	3167700.	91070907
SOURCE GROUP ID: LD7532					



Annual					
	1987	0.00240	340300.	3165700.	87123124
	1988	0.00340	340300.	3165700.	88123124
	1989	0.00346	343700.	3178300.	89123124
	1990	0.00221	340300.	3167700.	90123124
	1991	0.00230	340300.	3165700.	91123124
HIGH 24-Hour					
	1987	0.04216	340300.	3165700.	87122224
	1988	0.05198	343000.	3176200.	88112624
	1989	0.05751	340300.	3165700.	89100624
	1990	0.05223	341100.	3183400.	90021424
	1991	0.04241	340300.	3165700.	91072724
HIGH 8-Hour					
	1987	0.15458	340300.	3165700.	87122208
	1988	0.12447	343000.	3176200.	88082608
	1989	0.15490	340300.	3165700.	89100608
	1990	0.09785	341100.	3183400.	90021408
	1991	0.11473	340300.	3165700.	91030608
HIGH 3-Hour					
	1987	0.33197	340300.	3165700.	87011003
	1988	0.22157	343000.	3176200.	88060606
	1989	0.31784	340300.	3165700.	89030503
	1990	0.18970	340300.	3167700.	90112406
	1991	0.26537	340300.	3165700.	91052903
HIGH 1-Hour					
	1987	0.64237	340300.	3167700.	87072906
	1988	0.61886	340300.	3165700.	88092120
	1989	0.64128	340300.	3167700.	89091508
	1990	0.56909	340300.	3167700.	90112405
	1991	0.64096	340300.	3167700.	91070907
SOURCE GROUP ID: LD7595					
Annual					
	1987	0.00257	340300.	3165700.	87123124
	1988	0.00359	340300.	3165700.	88123124
	1989	0.00370	343700.	3178300.	89123124
	1990	0.00232	340300.	3167700.	90123124
	1991	0.00243	340300.	3165700.	91123124
HIGH 24-Hour					
	1987	0.04363	340300.	3165700.	87122224
	1988	0.05447	343000.	3176200.	88112624
	1989	0.06157	340300.	3165700.	89100624
	1990	0.05490	341100.	3183400.	90021424
	1991	0.04514	340300.	3165700.	91072724
HIGH 8-Hour					
	1987	0.15997	340300.	3165700.	87122208
	1988	0.12936	343000.	3176200.	88082608
	1989	0.16655	340300.	3165700.	89100608
	1990	0.10474	341100.	3183400.	90021408
	1991	0.12113	340300.	3165700.	91030608
HIGH 3-Hour					
	1987	0.34477	340300.	3165700.	87011003
	1988	0.23333	343000.	3176200.	88060606
	1989	0.33524	340300.	3165700.	89030503
	1990	0.19764	340300.	3167700.	90112406
	1991	0.27843	340300.	3165700.	91052903
HIGH 1-Hour					
	1987	0.67341	340300.	3167700.	87072906
	1988	0.64892	340300.	3165700.	88092120
	1989	0.67229	340300.	3167700.	89091508
	1990	0.59293	340300.	3167700.	90112405
	1991	0.67197	340300.	3167700.	91070907
SOURCE GROUP ID: LD5032					
Annual					
	1987	0.00283	340300.	3165700.	87123124
	1988	0.00395	340300.	3165700.	88123124
	1989	0.00411	343700.	3178300.	89123124
	1990	0.00250	340300.	3167700.	90123124
	1991	0.00269	340300.	3165700.	91123124
HIGH 24-Hour					
	1987	0.04616	343000.	3176200.	87061524
	1988	0.05954	340300.	3165700.	88073124
	1989	0.06847	340300.	3165700.	89100624
	1990	0.05951	341100.	3183400.	90021424
	1991	0.05015	340300.	3165700.	91072724
HIGH 8-Hour					
	1987	0.16884	340300.	3165700.	87122208
	1988	0.13754	343000.	3176200.	88082608

	1989	0.18727	340300.	3165700.	89100608
	1990	0.11674	341100.	3183400.	90021408
	1991	0.13208	340300.	3165700.	91030608
HIGH 3-Hour	1987	0.36917	343000.	3176200.	87061506
	1988	0.25366	343000.	3176200.	88060606
	1989	0.36515	340300.	3165700.	89030503
	1990	0.21083	340300.	3167700.	90112406
	1991	0.30086	340300.	3165700.	91052903
HIGH 1-Hour	1987	0.72602	340300.	3167700.	87072906
	1988	0.69989	340300.	3165700.	88092120
	1989	0.72500	340300.	3167700.	89091508
	1990	0.63248	340300.	3167700.	90112405
	1991	0.72471	340300.	3167700.	91070907
SOURCE GROUP ID:	LD5095				
Annual	1987	0.00292	340300.	3165700.	87123124
	1988	0.00405	340300.	3165700.	88123124
	1989	0.00422	343700.	3178300.	89123124
	1990	0.00257	340300.	3167700.	90123124
	1991	0.00276	340300.	3165700.	91123124
HIGH 24-Hour	1987	0.04770	343000.	3176200.	87061524
	1988	0.06160	340300.	3165700.	88073124
	1989	0.07109	340300.	3165700.	89100624
	1990	0.06123	341100.	3183400.	90021424
	1991	0.05209	340300.	3165700.	91072724
HIGH 8-Hour	1987	0.17200	340300.	3165700.	87122208
	1988	0.14046	343000.	3176200.	88082608
	1989	0.19510	340300.	3165700.	89100608
	1990	0.12125	341100.	3183400.	90021408
	1991	0.13616	340300.	3165700.	91030608
HIGH 3-Hour	1987	0.38154	343000.	3176200.	87061506
	1988	0.26119	343000.	3176200.	88060606
	1989	0.37619	340300.	3165700.	89030503
	1990	0.21558	340300.	3167700.	90112406
	1991	0.30910	340300.	3165700.	91052903
HIGH 1-Hour	1987	0.74511	340300.	3167700.	87072906
	1988	0.71840	340300.	3165700.	88092120
	1989	0.74412	340300.	3167700.	89091508
	1990	0.64674	340300.	3167700.	90112405
	1991	0.74383	340300.	3167700.	91070907

All receptor computations reported with respect to a user-specified origin

GRID 0.00 0.00  
DISCRETE 0.00 0.00

CO STARTING  
 CO TITLEONE 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
 CO TITLETWO NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1  
 CO MODELOPT DFAULT CONC RURAL  
 CO AVERTIME PERIOD 24 8 3 1  
 CO POLLUTID GEN  
 CO DCAYCOEF .000000  
 CO RUNORNOT RUN  
 CO FINISHED

SO STARTING

\*\* Source Location Cards:

\*\* SRCID SRCTYP XS YS ZS  
 \*\* MODELING ORIGIN CT NO.2 STACK LOCATION  
 \*\* CT STACK NUMBER CODE  
 \*\* -----  
 \*\* A - CT NO. 1  
 \*\* B - CT NO. 2  
 \*\* C - CT NO. 3

\*\* Source Location Cards:

SRCID	SRCTYP	XS (m)	YS (m)	ZS (m)
SO LOCATION BASE32A	POINT	419400	3069700	0.0
SO LOCATION BASE32B	POINT	419400	3069700	0.0
SO LOCATION BASE32C	POINT	419400	3069700	0.0
SO LOCATION BASE95A	POINT	419400	3069700	0.0
SO LOCATION BASE95B	POINT	419400	3069700	0.0
SO LOCATION BASE95C	POINT	419400	3069700	0.0
SO LOCATION LD7532A	POINT	419400	3069700	0.0
SO LOCATION LD7532B	POINT	419400	3069700	0.0
SO LOCATION LD7532C	POINT	419400	3069700	0.0
SO LOCATION LD7595A	POINT	419400	3069700	0.0
SO LOCATION LD7595B	POINT	419400	3069700	0.0
SO LOCATION LD7595C	POINT	419400	3069700	0.0
SO LOCATION LD5032A	POINT	419400	3069700	0.0
SO LOCATION LD5032B	POINT	419400	3069700	0.0
SO LOCATION LD5032C	POINT	419400	3069700	0.0
SO LOCATION LD5095A	POINT	419400	3069700	0.0
SO LOCATION LD5095B	POINT	419400	3069700	0.0
SO LOCATION LD5095C	POINT	419400	3069700	0.0

\*\* Source Parameter Cards:

POINT: SRCID	QS (g/s)	HS (m)	TS (K)	VS (m/s)	DS (m)
SO SRCPARAM BASE32A	3.334	18.3	853.0	36.2	6.4
SO SRCPARAM BASE32B	3.333	18.3	853.0	36.2	6.4
SO SRCPARAM BASE32C	3.333	18.3	853.0	36.2	6.4
SO SRCPARAM BASE95A	3.334	18.3	880.0	33.6	6.4
SO SRCPARAM BASE95B	3.333	18.3	880.0	33.6	6.4
SO SRCPARAM BASE95C	3.333	18.3	880.0	33.6	6.4
SO SRCPARAM LD7532A	3.334	18.3	902.0	30.5	6.4
SO SRCPARAM LD7532B	3.333	18.3	902.0	30.5	6.4
SO SRCPARAM LD7532C	3.333	18.3	902.0	30.5	6.4
SO SRCPARAM LD7595A	3.334	18.3	911.0	28.0	6.4
SO SRCPARAM LD7595B	3.333	18.3	911.0	28.0	6.4
SO SRCPARAM LD7595C	3.333	18.3	911.0	28.0	6.4
SO SRCPARAM LD5032A	3.334	18.3	853.0	25.3	6.4
SO SRCPARAM LD5032B	3.333	18.3	853.0	25.3	6.4
SO SRCPARAM LD5032C	3.333	18.3	853.0	25.3	6.4
SO SRCPARAM LD5095A	3.334	18.3	840.0	24.3	6.4
SO SRCPARAM LD5095B	3.333	18.3	840.0	24.3	6.4
SO SRCPARAM LD5095C	3.333	18.3	840.0	24.3	6.4

SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	14.63	14.63
SO BUILDHGT	BASE32A-BASE95A	14.63	14.63	14.63	14.63	0.00	14.33

SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32A-BASE95A	0.00	0.00	0.00	0.00	14.33	14.33
SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	BASE32A-BASE95A	12.74	14.10	15.03	15.50	24.40	23.57
SO BUILDWID	BASE32A-BASE95A	23.32	23.54	23.80	23.33	0.00	15.03
SO BUILDWID	BASE32A-BASE95A	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	BASE32A-BASE95A	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32A-BASE95A	0.00	0.00	0.00	0.00	14.10	15.03
SO BUILDWID	BASE32A-BASE95A	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32B-BASE95B	14.33	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32B-BASE95B	0.00	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	BASE32B-BASE95B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32B-BASE95B	14.10	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	BASE32B-BASE95B	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	BASE32B-BASE95B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32B-BASE95B	0.00	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	BASE32B-BASE95B	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32C-BASE95C	14.33	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32C-BASE95C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32C-BASE95C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32C-BASE95C	14.10	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	15.28	14.37	13.02	11.28	9.20
SO BUILDWID	BASE32C-BASE95C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	BASE32C-BASE95C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	15.28	14.37	13.02	11.28	9.20
**							
SO BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	14.63	14.63
SO BUILDHGT	LD7532A-LD7595A	14.63	14.63	14.63	14.63	0.00	14.33
SO BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532A-LD7595A	0.00	0.00	0.00	0.00	14.33	14.33
SO BUILDHGT	LD7532A-LD7595A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	LD7532A-LD7595A	12.74	14.10	15.03	15.50	24.40	23.57
SO BUILDWID	LD7532A-LD7595A	23.32	23.54	23.80	23.33	0.00	15.03
SO BUILDWID	LD7532A-LD7595A	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	LD7532A-LD7595A	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532A-LD7595A	0.00	0.00	0.00	0.00	14.10	15.03
SO BUILDWID	LD7532A-LD7595A	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532B-LD7595B	14.33	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532B-LD7595B	0.00	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	LD7532B-LD7595B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	LD7532B-LD7595B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532B-LD7595B	14.10	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	LD7532B-LD7595B	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	LD7532B-LD7595B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532B-LD7595B	0.00	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	LD7532B-LD7595B	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	LD7532C-LD7595C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532C-LD7595C	14.33	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD7532C-LD7595C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	LD7532C-LD7595C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD7532C-LD7595C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD7532C-LD7595C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD7532C-LD7595C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532C-LD7595C	14.10	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD7532C-LD7595C	0.00	15.28	14.37	13.02	11.28	9.20
SO BUILDWID	LD7532C-LD7595C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD7532C-LD7595C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD7532C-LD7595C	0.00	15.28	14.37	13.02	11.28	9.20
**							
SO BUILDHGT	LD5032A-LD5095A	14.33	14.33	14.33	14.33	14.63	14.63

SO BUILDHGT	LD5032A-LD5095A	14.63	14.63	14.63	14.63	0.00	14.33
SO BUILDHGT	LD5032A-LD5095A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032A-LD5095A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032A-LD5095A	0.00	0.00	0.00	0.00	14.33	14.33
SO BUILDHGT	LD5032A-LD5095A	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	LD5032A-LD5095A	12.74	14.10	15.03	15.50	24.40	23.57
SO BUILDWID	LD5032A-LD5095A	23.32	23.54	23.80	23.33	0.00	15.03
SO BUILDWID	LD5032A-LD5095A	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	LD5032A-LD5095A	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032A-LD5095A	0.00	0.00	0.00	0.00	14.10	15.03
SO BUILDWID	LD5032A-LD5095A	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	LD5032B-LD5095B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032B-LD5095B	14.33	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	LD5032B-LD5095B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032B-LD5095B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032B-LD5095B	0.00	0.00	0.00	0.00	0.00	14.33
SO BUILDHGT	LD5032B-LD5095B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDWID	LD5032B-LD5095B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032B-LD5095B	14.10	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	LD5032B-LD5095B	15.50	15.50	15.03	14.10	11.18	9.10
SO BUILDWID	LD5032B-LD5095B	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032B-LD5095B	0.00	0.00	0.00	0.00	0.00	15.03
SO BUILDWID	LD5032B-LD5095B	15.50	15.50	15.03	14.10	11.18	9.10
**							
SO BUILDHGT	LD5032C-LD5095C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032C-LD5095C	14.33	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032C-LD5095C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	LD5032C-LD5095C	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032C-LD5095C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032C-LD5095C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032C-LD5095C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032C-LD5095C	14.10	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032C-LD5095C	0.00	15.28	14.37	13.02	11.28	9.20
SO BUILDWID	LD5032C-LD5095C	12.74	14.10	15.03	15.50	15.50	15.03
SO BUILDWID	LD5032C-LD5095C	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032C-LD5095C	0.00	15.28	14.37	13.02	11.28	9.20

\*\*  
 SO EMISUNIT .100000E+07 (GRAMS/SEC) (MICROGRAMS/CUBIC-METER)

SO SRCGROUP	BASE32	BASE32A	BASE32B	BASE32C
SO SRCGROUP	BASE95	BASE95A	BASE95B	BASE95C
SO SRCGROUP	LD7532	LD7532A	LD7532B	LD7532C
SO SRCGROUP	LD7595	LD7595A	LD7595B	LD7595C
SO SRCGROUP	LD5032	LD5032A	LD5032B	LD5032C
SO SRCGROUP	LD5095	LD5095A	LD5095B	LD5095C

SO FINISHED

\*\*

RE STARTING

\*\*

	UTM(m)	UTM(m)
RE DISCCART	340300	3165700
RE DISCCART	340300	3167700
RE DISCCART	340300	3169800
RE DISCCART	340700	3171900
RE DISCCART	342000	3174000
RE DISCCART	343000	3176200
RE DISCCART	343700	3178300
RE DISCCART	342400	3180600
RE DISCCART	341100	3183400
RE DISCCART	339000	3183400
RE DISCCART	336500	3183400
RE DISCCART	334000	3183400
RE DISCCART	331500	3183400

RE FINISHED

\*\*

ME STARTING

ME INPUTFIL P:\MET\TPATPA87.MET

ME ANEMHGHT 22 FEET

ME SURFDATA 12842 1987 TAMPA

ME UAIRDATA 12842 1987 TAMPA

ME WINDCATS 1.54 3.09 5.14 8.23 10.80

ME FINISHED

\*\*

OU STARTING









\*\*\* ISCS3 - VERSION 99155 \*\*\* \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00 \*\*\*  
\*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
\*\*\* 15:05:  
PAGE

\*\*MODELOPTs:  
CONC

RURAL FLAT DFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: LD7532C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0
13	0.0,	0.0,	0	14	6.7,	15.3,	0	15	6.7,	14.4,	0	16	6.7,	13.0,	0	17	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0
31	0.0,	0.0,	0	32	6.7,	15.3,	0	33	6.7,	14.4,	0	34	6.7,	13.0,	0	35	6.7,	9

SOURCE ID: LD7595A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.6,	23
7	14.6,	23.3,	0	8	14.6,	23.5,	0	9	14.6,	23.8,	0	10	14.6,	23.3,	0	11	0.0,	15
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	9

SOURCE ID: LD7595B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	15
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	9

SOURCE ID: LD7595C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	15
13	0.0,	0.0,	0	14	6.7,	15.3,	0	15	6.7,	14.4,	0	16	6.7,	13.0,	0	17	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0
31	0.0,	0.0,	0	32	6.7,	15.3,	0	33	6.7,	14.4,	0	34	6.7,	13.0,	0	35	6.7,	9

\*\*\* ISCS3 - VERSION 99155 \*\*\* \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00 \*\*\*  
\*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
\*\*\* 15:05:  
PAGE

\*\*MODELOPTs:  
CONC

RURAL FLAT DFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: LD5032A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.6,	23
7	14.6,	23.3,	0	8	14.6,	23.5,	0	9	14.6,	23.8,	0	10	14.6,	23.3,	0	11	0.0,	15
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	9

SOURCE ID: LD5032B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	B
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	15
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	9
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15

25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	14.3,	15
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9

SOURCE ID: LD5032C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	15	
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	0.0,	0	
13	0.0,	0.0,	0	14	6.7,	15.3,	0	15	6.7,	14.4,	0	16	6.7,	13.0,	0	17	6.7,	11.3,	0	18	6.7,	9	
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15	
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	0.0,	0	
31	0.0,	0.0,	0	32	6.7,	15.3,	0	33	6.7,	14.4,	0	34	6.7,	13.0,	0	35	6.7,	11.3,	0	36	6.7,	9	

SOURCE ID: LD5095A

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.6,	24.4,	0	6	14.6,	23	
7	14.6,	23.3,	0	8	14.6,	23.5,	0	9	14.6,	23.8,	0	10	14.6,	23.3,	0	11	0.0,	0.0,	0	12	14.3,	15	
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	9	
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15	
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	14.3,	14.1,	0	30	14.3,	15	
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9	

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00      \*\*\*      04/21  
 \*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1      \*\*\*      15:05:  
 \*\*MODELOPTS:      PAGE

CONC      RURAL    FLAT      DFAULT

\*\*\* DIRECTION SPECIFIC BUILDING DIMENSIONS \*\*\*

SOURCE ID: LD5095B

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	15	
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	14.3,	15	
13	14.3,	15.5,	0	14	14.3,	15.5,	0	15	14.3,	15.0,	0	16	14.3,	14.1,	0	17	6.7,	11.2,	0	18	6.7,	9	
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15	
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	14.3,	15	
31	14.3,	15.5,	0	32	14.3,	15.5,	0	33	14.3,	15.0,	0	34	14.3,	14.1,	0	35	6.7,	11.2,	0	36	6.7,	9	

SOURCE ID: LD5095C

IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK	IFV	BH	BW	WAK
1	14.3,	12.7,	0	2	14.3,	14.1,	0	3	14.3,	15.0,	0	4	14.3,	15.5,	0	5	14.3,	15.5,	0	6	14.3,	15	
7	14.3,	14.1,	0	8	0.0,	0.0,	0	9	0.0,	0.0,	0	10	0.0,	0.0,	0	11	0.0,	0.0,	0	12	0.0,	0	
13	0.0,	0.0,	0	14	6.7,	15.3,	0	15	6.7,	14.4,	0	16	6.7,	13.0,	0	17	6.7,	11.3,	0	18	6.7,	9	
19	14.3,	12.7,	0	20	14.3,	14.1,	0	21	14.3,	15.0,	0	22	14.3,	15.5,	0	23	14.3,	15.5,	0	24	14.3,	15	
25	0.0,	0.0,	0	26	0.0,	0.0,	0	27	0.0,	0.0,	0	28	0.0,	0.0,	0	29	0.0,	0.0,	0	30	0.0,	0	
31	0.0,	0.0,	0	32	6.7,	15.3,	0	33	6.7,	14.4,	0	34	6.7,	13.0,	0	35	6.7,	11.3,	0	36	6.7,	9	

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00      \*\*\*      04/21  
 \*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1      \*\*\*      15:05:  
 \*\*MODELOPTS:      PAGE

CONC      RURAL    FLAT      DFAULT

\*\*\* DISCRETE CARTESIAN RECEPTORS \*\*\*  
 (X-COORD, Y-COORD, ZELEV, ZFLAG)  
 (METERS)

( 340300.0, 3165700.0, 0.0, 0.0);	( 340300.0, 3167700.0, 0.0, 0.0);
( 340300.0, 3169800.0, 0.0, 0.0);	( 340700.0, 3171900.0, 0.0, 0.0);
( 342000.0, 3174000.0, 0.0, 0.0);	( 343000.0, 3176200.0, 0.0, 0.0);
( 343700.0, 3178300.0, 0.0, 0.0);	( 342400.0, 3180600.0, 0.0, 0.0);
( 341100.0, 3183400.0, 0.0, 0.0);	( 339000.0, 3183400.0, 0.0, 0.0);
( 336500.0, 3183400.0, 0.0, 0.0);	( 334000.0, 3183400.0, 0.0, 0.0);
( 331500.0, 3183400.0, 0.0, 0.0);	

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00      \*\*\*      04/21  
 \*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1      \*\*\*      15:05:  
 \*\*MODELOPTS:      PAGE

CONC      RURAL    FLAT      DFAULT



87	01	01	12	116.0	6.17	287.0	4	1182.0	1182.0	0.0000	0.0	0.0000	0	0.00
87	01	01	13	133.0	7.20	287.6	4	1235.0	1235.0	0.0000	0.0	0.0000	0	0.00
87	01	01	14	119.0	7.72	287.6	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	15	132.0	7.20	288.2	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	16	134.0	7.72	289.3	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	17	141.0	7.20	288.2	4	1288.0	1288.0	0.0000	0.0	0.0000	0	0.00
87	01	01	18	137.0	5.14	287.6	5	1286.4	1238.1	0.0000	0.0	0.0000	0	0.00
87	01	01	19	144.0	3.60	286.5	5	1281.2	1078.6	0.0000	0.0	0.0000	0	0.00
87	01	01	20	117.0	2.06	285.4	6	1276.0	919.0	0.0000	0.0	0.0000	0	0.00
87	01	01	21	110.0	1.54	284.8	7	1270.9	759.5	0.0000	0.0	0.0000	0	0.00
87	01	01	22	112.0	0.00	283.7	7	1265.7	600.0	0.0000	0.0	0.0000	0	0.00
87	01	01	23	120.0	2.57	283.7	6	1260.5	440.5	0.0000	0.0	0.0000	0	0.00
87	01	01	24	130.0	1.54	282.6	7	1255.4	281.0	0.0000	0.0	0.0000	0	0.00

\*\*\* NOTES: STABILITY CLASS 1=A, 2=B, 3=C, 4=D, 5=E AND 6=F.  
FLOW VECTOR IS DIRECTION TOWARD WHICH WIND IS BLOWING.

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
\*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
\*\*\* 15:05:  
PAGE

\*\*MODELOPTs:  
CONC

RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF MAXIMUM PERIOD ( 8760 HRS) RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

GROUP ID	AVERAGE CONC	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWORK GRID-ID
BASE32	1ST HIGHEST VALUE IS	0.00215 AT ( 340300.00, 3165700.00,	0.00, 0.00) DC	NA
	2ND HIGHEST VALUE IS	0.00203 AT ( 340300.00, 3167700.00,	0.00, 0.00) DC	NA
	3RD HIGHEST VALUE IS	0.00190 AT ( 340300.00, 3169800.00,	0.00, 0.00) DC	NA
BASE95	1ST HIGHEST VALUE IS	0.00225 AT ( 340300.00, 3165700.00,	0.00, 0.00) DC	NA
	2ND HIGHEST VALUE IS	0.00211 AT ( 340300.00, 3167700.00,	0.00, 0.00) DC	NA
	3RD HIGHEST VALUE IS	0.00198 AT ( 340300.00, 3169800.00,	0.00, 0.00) DC	NA
LD7532	1ST HIGHEST VALUE IS	0.00240 AT ( 340300.00, 3165700.00,	0.00, 0.00) DC	NA
	2ND HIGHEST VALUE IS	0.00226 AT ( 340300.00, 3167700.00,	0.00, 0.00) DC	NA
	3RD HIGHEST VALUE IS	0.00212 AT ( 340300.00, 3169800.00,	0.00, 0.00) DC	NA
LD7595	1ST HIGHEST VALUE IS	0.00257 AT ( 340300.00, 3165700.00,	0.00, 0.00) DC	NA
	2ND HIGHEST VALUE IS	0.00241 AT ( 340300.00, 3167700.00,	0.00, 0.00) DC	NA
	3RD HIGHEST VALUE IS	0.00226 AT ( 340300.00, 3169800.00,	0.00, 0.00) DC	NA
LD5032	1ST HIGHEST VALUE IS	0.00283 AT ( 340300.00, 3165700.00,	0.00, 0.00) DC	NA
	2ND HIGHEST VALUE IS	0.00264 AT ( 340300.00, 3167700.00,	0.00, 0.00) DC	NA
	3RD HIGHEST VALUE IS	0.00247 AT ( 340300.00, 3169800.00,	0.00, 0.00) DC	NA
LD5095	1ST HIGHEST VALUE IS	0.00292 AT ( 340300.00, 3165700.00,	0.00, 0.00) DC	NA
	2ND HIGHEST VALUE IS	0.00272 AT ( 340300.00, 3167700.00,	0.00, 0.00) DC	NA
	3RD HIGHEST VALUE IS	0.00254 AT ( 340300.00, 3169800.00,	0.00, 0.00) DC	NA

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
GP = GRIDPOLR  
DC = DISCCART  
DP = DISCPOLR  
BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\*      \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
\*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
\*\*\* 15:05:  
PAGE

\*\*MODELOPTs:  
CONC

RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF HIGHEST 24-HR RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

GROUP ID	AVERAGE CONC	DATE (YYMMDDHH)	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWORK GRID-ID
BASE32	HIGH 1ST HIGH VALUE IS	0.03953c ON 87122224:	AT ( 340300.00, 3165700.00,	0.00, 0.00) DC	NA

BASE95 HIGH 1ST HIGH VALUE IS 0.04061c ON 87122224: AT ( 340300.00, 3165700.00, 0.00, 0.00) DC NA  
 LD7532 HIGH 1ST HIGH VALUE IS 0.04216c ON 87122224: AT ( 340300.00, 3165700.00, 0.00, 0.00) DC NA  
 LD7595 HIGH 1ST HIGH VALUE IS 0.04363c ON 87122224: AT ( 340300.00, 3165700.00, 0.00, 0.00) DC NA  
 LD5032 HIGH 1ST HIGH VALUE IS 0.04616 ON 87061524: AT ( 343000.00, 3176200.00, 0.00, 0.00) DC NA  
 LD5095 HIGH 1ST HIGH VALUE IS 0.04770 ON 87061524: AT ( 343000.00, 3176200.00, 0.00, 0.00) DC NA

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
 GP = GRIDPOLR  
 DC = DISCCART  
 DP = DISCPOLR  
 BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\* \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
 \*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
 \*\*\* 15:05:  
 PAGE

\*\*MODELOPTs:  
 CONC RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF HIGHEST 8-HR RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

GROUP ID	AVERAGE CONC	DATE (YYMMDDHH)	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWORK GRID-I
BASE32 HIGH 1ST HIGH VALUE IS	0.14493c	ON 87122208: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
BASE95 HIGH 1ST HIGH VALUE IS	0.14889c	ON 87122208: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD7532 HIGH 1ST HIGH VALUE IS	0.15458c	ON 87122208: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD7595 HIGH 1ST HIGH VALUE IS	0.15997c	ON 87122208: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD5032 HIGH 1ST HIGH VALUE IS	0.16884c	ON 87122208: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD5095 HIGH 1ST HIGH VALUE IS	0.17200c	ON 87122208: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA

\*\*\* RECEPTOR TYPES: GC = GRIDCART  
 GP = GRIDPOLR  
 DC = DISCCART  
 DP = DISCPOLR  
 BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\* \*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00  
 \*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21  
 \*\*\* 15:05:  
 PAGE

\*\*MODELOPTs:  
 CONC RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF HIGHEST 3-HR RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

GROUP ID	AVERAGE CONC	DATE (YYMMDDHH)	RECEPTOR (XR, YR, ZELEV, ZFLAG)	OF TYPE	NETWORK GRID-I
BASE32 HIGH 1ST HIGH VALUE IS	0.30919	ON 87011003: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
BASE95 HIGH 1ST HIGH VALUE IS	0.31851	ON 87011003: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD7532 HIGH 1ST HIGH VALUE IS	0.33197	ON 87011003: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD7595 HIGH 1ST HIGH VALUE IS	0.34477	ON 87011003: AT (	340300.00, 3165700.00, 0.00, 0.00)	DC	NA
LD5032 HIGH 1ST HIGH VALUE IS	0.36917	ON 87061506: AT (	343000.00, 3176200.00, 0.00, 0.00)	DC	NA
LD5095 HIGH 1ST HIGH VALUE IS	0.38154	ON 87061506: AT (	343000.00, 3176200.00, 0.00, 0.00)	DC	NA

\*\*\* RECEPTOR TYPES: GC = GRIDCART

GP = GRIDPOLR
DC = DISCCART
DP = DISCPOLR
BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\*
\*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00
\*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21
\*\*\* 15:05:
PAGE

\*\*MODELOPTs:
CONC RURAL FLAT DFAULT

\*\*\* THE SUMMARY OF HIGHEST 1-HR RESULTS \*\*\*

\*\* CONC OF GEN IN (MICROGRAMS/CUBIC-METER) \*\*

Table with columns: GROUP ID, AVERAGE CONC, DATE (YYMMDDHH), RECEPTOR (XR, YR, ZELEV, ZFLAG), OF TYPE, NETWORK GRID-I. Rows include BASE32, BASE95, LD7532, LD7595, LD5032, LD5095.

\*\*\* RECEPTOR TYPES:
GC = GRIDCART
GP = GRIDPOLR
DC = DISCCART
DP = DISCPOLR
BD = BOUNDARY

\*\*\* ISCST3 - VERSION 99155 \*\*\*
\*\*\* 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/21/00
\*\*\* NAT GAS, GEN. EM. RATES, 3 LOADS / 2 TEMP. CLASS 1

\*\*\* 04/21
\*\*\* 15:05:
PAGE

\*\*MODELOPTs:
CONC RURAL FLAT DFAULT

\*\*\* Message Summary : ISCST3 Model Execution \*\*\*

----- Summary of Total Messages -----

A Total of 0 Fatal Error Message(s)
A Total of 0 Warning Message(s)
A Total of 531 Informational Message(s)
A Total of 531 Calm Hours Identified

\*\*\*\*\* FATAL ERROR MESSAGES \*\*\*\*\*
\*\*\* NONE \*\*\*

\*\*\*\*\* WARNING MESSAGES \*\*\*\*\*
\*\*\* NONE \*\*\*

\*\*\*\*\*
\*\*\* ISCST3 Finishes Successfully \*\*\*
\*\*\*\*\*

TABLE OF REFINEMENT SUMMARY FILES

ISCSOB3 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :RRSANC2.090

First title for last output file is: 1990 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/25/00  
Second title for last output file is: FUEL OIL, SO2 ANNUAL EM. RATES, BASE / 32of 2ND REFINE CLASS 2

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
----------------	------	-----------------	-----------------------	----------------------	-----------------------------

SOURCE GROUP ID: BASE32  
Annual

	1990	0.07101	254.	14800.	90123124
All receptor computations reported with respect to a user-specified origin					
GRID	0.00	0.00			
DISCRETE	0.00	0.00			

ISCSOB3 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :RRS24C2.089

First title for last output file is: 1989 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/25/00  
Second title for last output file is: FUEL OIL, SO2 24 HR EM. RATES, BASE/32of 2ND REFINE CLASS 2

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
----------------	------	-----------------	-----------------------	----------------------	-----------------------------

SOURCE GROUP ID: BASE32  
HIGH 24-Hour

	1989	0.95574	188.	20000.	89120424
All receptor computations reported with respect to a user-specified origin					
GRID	0.00	0.00			
DISCRETE	0.00	0.00			

ISCSOB3 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :RS03C2.089

First title for last output file is: 1989 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/25/00  
Second title for last output file is: FUEL OIL, SO2 3 HR. RATES, 50% LOAD/32of REFINE CLASS 2

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
----------------	------	-----------------	-----------------------	----------------------	-----------------------------

SOURCE GROUP ID: LD5032  
HIGH 3-Hour

	1989	4.22211	332.	1500.	89062212
All receptor computations reported with respect to a user-specified origin					
GRID	0.00	0.00			
DISCRETE	0.00	0.00			

ISCSOB3 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :RPANC2.090

First title for last output file is: 1990 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/25/00  
Second title for last output file is: FUEL OIL, PM ANNUAL EM. RATES, 50% LOAD/95of REFINE CLASS 2

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
----------------	------	-----------------	-----------------------	----------------------	-----------------------------

SOURCE GROUP ID: LD5095  
Annual

	1990	0.02367	254.	10300.	90123124
All receptor computations reported with respect to a user-specified origin					
GRID	0.00	0.00			
DISCRETE	0.00	0.00			

=====
  
ISCBOB3 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :RP24C2.088

First title for last output file is: 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/25/00

Second title for last output file is: FUEL OIL, PM 24 HR EM. RATES, 50% LOAD/95of REFINE CLASS 2

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
----------------	------	-----------------	-----------------------	----------------------	-----------------------------

-----
  
SOURCE GROUP ID: LD5095  
HIGH 24-Hour

	1988	0.28030	164.	1600.	88080724
--	------	---------	------	-------	----------

All receptor computations reported with respect to a user-specified origin

GRID	0.00	0.00			
DISCRETE	0.00	0.00			

=====
  
ISCBOB3 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :RRNANC2.090

First title for last output file is: 1990 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/25/00

Second title for last output file is: FUEL OIL, NO2 ANNUAL EM. RATES, BASE/32of 2ND REFINE CLASS 2

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
----------------	------	-----------------	-----------------------	----------------------	-----------------------------

-----
  
SOURCE GROUP ID: BASE32  
Annual

	1990	0.23385	254.	14800.	90123124
--	------	---------	------	--------	----------

All receptor computations reported with respect to a user-specified origin

GRID	0.00	0.00			
DISCRETE	0.00	0.00			

=====
  
ISCBOB3 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :RC08C2.088

First title for last output file is: 1988 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/25/00

Second title for last output file is: FUEL OIL, CO 8 HR EM. RATES, 50% LOAD/95of REFINE CLASS 2

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
----------------	------	-----------------	-----------------------	----------------------	-----------------------------

-----
  
SOURCE GROUP ID: LD5095  
HIGH 8-Hour

	1988	1.44676	164.	1600.	88080716
--	------	---------	------	-------	----------

All receptor computations reported with respect to a user-specified origin

GRID	0.00	0.00			
DISCRETE	0.00	0.00			

=====
  
ISCBOB3 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :RC01C2.087

First title for last output file is: 1987 DECKER, FT. MEADE 3 CTS/SIMPLE CYCLE 04/25/00

Second title for last output file is: FUEL OIL, CO 1 HR EM. RATES, 50% LOAD/95of REFINE CLASS 2

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
----------------	------	-----------------	-----------------------	----------------------	-----------------------------

-----
  
SOURCE GROUP ID: LD5095  
HIGH 1-Hour

	1987	5.56334	110.	1400.	87061811
--	------	---------	------	-------	----------

All receptor computations reported with respect to a user-specified origin

GRID	0.00	0.00			
DISCRETE	0.00	0.00			





DECKER FT MEADE AGRV IMPACTS AT CHASSAHOWITZKA NWA, SO2 4/24/00  
 RECEPTORS AT CHASSAHOWITZKA NWA, ALL AVERAGING ITMES, CALPOST  
 3 SIMPLE-CYCLE CTS, NATURAL GAS, BASE LOAD, 32 DEGREES  
 ----- Run title (3 lines) -----

CALPOST MODEL CONTROL FILE  
 -----

INPUT GROUP: 0 -- Input and Output File Names  
 -----

Input Files  
 -----

File	Default File Name	
Conc/Dep Flux File	MODEL.DAT	! MODDAT =CALPUFF.CON !
Relative Humidity File	VISB.DAT	* VISDAT = *
Background Data File	BACK.DAT	*BACKDAT = *
Transmissometer/ Nephelometer Data File	VSRN.DAT	*VSRDAT = *

Output Files  
 -----

File	Default File Name	
List File	CALPOST.LST	! PSTLST =CALPOST.LST !

Pathname for Timeseries Files (blank) \* TSPATH = \*  
 (activate with exclamation points only if  
 providing NON-BLANK character string)

Pathname for Plot Files (blank) \* PLPATH = \*  
 (activate with exclamation points only if  
 providing NON-BLANK character string)

User Character String (U) to augment default filenames  
 (activate with exclamation points only if  
 providing NON-BLANK character string)

Timeseries	TSttUUUU.DAT	* TSUNAM = *
------------	--------------	--------------

Top Nth Rank Plot	RttUUUUU.DAT or RttiiUUU.GRD	* TUNAM = *
-------------------	---------------------------------	-------------

Exceedance Plot	XttUUUUU.DAT or XttUUUUU.GRD	* XUNAM = *
-----------------	---------------------------------	-------------

Echo Plot (Specific Days)	jjjtthHU.DAT or jjjtthHU.GRD	* EUNAM = *
------------------------------	---------------------------------	-------------

Visibility Plot (Daily Peak Summary)	V24UUUUU.DAT	* VUNAM = *
---	--------------	-------------

-----  
 All file names will be converted to lower case if LCFILES = T  
 Otherwise, if LCFILES = F, file names will be converted to UPPER CASE  
 T = lower case ! LCFILES = T !  
 F = UPPER CASE

NOTE: (1) file/path names can be up to 70 characters in length  
 NOTE: (2) Filenames for ALL PLOT and TIMESERIES FILES are constructed  
 using a template that includes a pathname, user-supplied  
 character(s), and fixed strings (tt,ii,jjj, and hh), where  
 tt = Averaging Period (e.g. 03)  
 ii = Rank (e.g. 02)  
 jjj= Julian Day  
 hh = Hour(ending)  
 are determined internally based on selections made below.  
 If a path or user-supplied character(s) are supplied, each  
 must contain at least 1 non-blank character.

!END!  
 -----



--Specific gridded receptors can also be excluded from CALPOST processing by filling a processing grid array with 0s and 1s. If the processing flag for receptor index (i,j) is 1 (ON), that receptor will be processed if it lies within the range delineated by IBGRID, JBGRID, IEGRID, JEGRID and if LG=T. If it is 0 (OFF), it will not be processed in the run. By default, all array values are set to 1 (ON).

Number of gridded receptor rows provided in Subgroup (1a) to identify specific gridded receptors to process  
(NGONOFF) -- Default: 0 ! NGONOFF = 0 !

!END!

-----  
Subgroup (1a) -- Specific gridded receptors included/excluded  
-----

Specific gridded receptors are excluded from CALPOST processing by filling a processing grid array with 0s and 1s. A total of NGONOFF lines are read here. Each line corresponds to one 'row' in the sampling grid, starting with the NORTHERNMOST row that contains receptors that you wish to exclude, and finishing with row 1 to the SOUTH (no intervening rows may be skipped). Within a row, each receptor position is assigned either a 0 or 1, starting with the westernmost receptor.

0 = gridded receptor not processed  
1 = gridded receptor processed

Repeated value notation may be used to select blocks of receptors:  
23\*1, 15\*0, 12\*1

Because all values are initially set to 1, any receptors north of the first row entered, or east of the last value provided in a row, remain ON.

(NGXRECP) -- Default: 1

-----  
INPUT GROUP: 2 -- Visibility Parameters (ASPEC = VISIB)  
-----

Maximum relative humidity (%) used in particle growth curve  
(RHMAX) -- Default: 98 ! RHMAX = 0.0 !

Modeled species to be included in computing the light extinction  
Include SULFATE? (LVSO4) -- Default: T ! LVSO4 = T !  
Include NITRATE? (LVNO3) -- Default: T ! LVNO3 = T !  
Include ORGANIC CARBON? (LVOC) -- Default: T ! LVOC = T !  
Include COARSE PARTICLES? (LVPMC) -- Default: T ! LVPMC = T !  
Include FINE PARTICLES? (LVPMF) -- Default: T ! LVPMF = T !

And, when ranking for TOP-N, TOP-50, and Exceedance tables,  
Include BACKGROUND? (LVBK) -- Default: T ! LVBK = T !

Species name used for particulates in MODEL.DAT file  
COARSE (SPECPMC) -- Default: PMC ! SPECPMC = PMC !  
FINE (SPECPMF) -- Default: PMF ! SPECPMF = PMF !

Extinction Efficiency (1/Mm per ug/m\*\*3)  
-----

MODELED particulate species:  
PM COARSE (EELPMC) -- Default: 0.6 ! EELPMC = 0.6 !  
PM FINE (EELPMF) -- Default: 1.0 ! EELPMF = 1.0 !  
BACKGROUND particulate species:  
PM COARSE (EELPMCBK) -- Default: 0.6 ! EELPMCBK = 0.6 !  
Other species:  
AMMONIUM SULFATE (EESO4) -- Default: 3.0 ! EESO4 = 3.0 !  
AMMONIUM NITRATE (EENO3) -- Default: 3.0 ! EENO3 = 3.0 !  
ORGANIC CARBON (EEOC) -- Default: 4.0 ! EEOC = 4.0 !  
SOIL (EESOIL) -- Default: 1.0 ! EESOIL = 1.0 !  
ELEMENTAL CARBON (EEEC) -- Default: 10. ! EEEC = 10.0 !

## Background Extinction Computation

Method used for background light extinction

(MVISBK) -- Default: 6 ! MVISBK = 2 !

- 1 = Supply single light extinction and hygroscopic fraction
  - IWAQM (1993) RH adjustment applied to hygroscopic background and modeled sulfate and nitrate
- 2 = Compute extinction from speciated PM measurements (A)
  - Hourly RH adjustment applied to observed and modeled sulfate and nitrate
  - RH factor is capped at RHMAX
- 3 = Compute extinction from speciated PM measurements (B)
  - Hourly RH adjustment applied to observed and modeled sulfate and nitrate
  - Receptor-hour excluded if RH>RHMAX
  - Receptor-day excluded if fewer than 6 valid receptor-hours
- 4 = Read hourly transmissometer background extinction measurements
  - Hourly RH adjustment applied to modeled sulfate and nitrate
  - Hour excluded if measurement invalid (missing, interference, or large RH)
  - Receptor-hour excluded if RH>RHMAX
  - Receptor-day excluded if fewer than 6 valid receptor-hours
- 5 = Read hourly nephelometer background extinction measurements
  - Rayleigh extinction value (BEXTRAY) added to measurement
  - Hourly RH adjustment applied to modeled sulfate and nitrate
  - Hour excluded if measurement invalid (missing, interference, or large RH)
  - Receptor-hour excluded if RH>RHMAX
  - Receptor-day excluded if fewer than 6 valid receptor-hours
- 6 = Compute extinction from speciated PM measurements
  - FLAG RH adjustment factor applied to observed and modeled sulfate and nitrate

Additional inputs used for MVISBK = 1:

-----  
Background light extinction (1/Mm)

(BEXTBK) -- No default ! BEXTBK = 0.0 !

Percentage of particles affected by relative humidity

(RHFAC) -- No default ! RHFAC = 0.0 !

Additional inputs used for MVISBK = 6:

-----  
Extinction coefficients for hygroscopic species (modeled and background) are computed using a monthly RH adjustment factor in place of an hourly RH factor (VISB.DAT file is NOT needed). Enter the 12 monthly factors here (RHFAC). Month 1 is January.(RHFAC) -- No default ! RHFAC = 0.0, 0.0, 0.0, 0.0,  
0.0, 0.0, 0.0, 0.0,  
0.0, 0.0, 0.0, 0.0 !

Additional inputs used for MVISBK = 2,3,6:

-----  
Background extinction coefficients are computed from monthly CONCENTRATIONS of ammonium sulfate (BKS04), ammonium nitrate (BKNO3), coarse particulates (BKPMC), organic carbon (BKOC), soil (BKSOIL), and elemental carbon (BKEC). Month 1 is January. (ug/m\*\*3)(BKS04) -- No default ! BKS04 = 0.0, 0.0, 0.0, 0.0,  
0.0, 0.0, 0.0, 0.0,  
0.0, 0.0, 0.0, 0.0 !(BKNO3) -- No default ! BKNO3 = 0.0, 0.0, 0.0, 0.0,  
0.0, 0.0, 0.0, 0.0,  
0.0, 0.0, 0.0, 0.0 !(BKPMC) -- No default ! BKPMC = 0.0, 0.0, 0.0, 0.0,  
0.0, 0.0, 0.0, 0.0,  
0.0, 0.0, 0.0, 0.0 !(BKOC) -- No default ! BKOC = 0.0, 0.0, 0.0, 0.0,  
0.0, 0.0, 0.0, 0.0,  
0.0, 0.0, 0.0, 0.0 !(BKSOIL) -- No default ! BKSOIL = 0.0, 0.0, 0.0, 0.0,  
0.0, 0.0, 0.0, 0.0,  
0.0, 0.0, 0.0, 0.0 !

(BKEC) -- No default ! BKEC = 0.0, 0.0, 0.0, 0.0,

0.0, 0.0, 0.0, 0.0,  
0.0, 0.0, 0.0, 0.0 !

Additional inputs used for MVISBK = 2,3,5,6:

-----  
Extinction due to Rayleigh scattering is added (1/Mm)  
(BEXTRAY) -- Default: 10.0 ! BEXTRAY = 0.0 !

!END!  
-----

INPUT GROUP: 3 -- Output options  
-----

Output Units  
-----

Units for All Output	(IPRTU) -- Default: 1	! IPRTU = 3	!
for	for		
Concentration	Deposition		
1 = g/m**3	g/m**2/s		
2 = mg/m**3	mg/m**2/s		
3 = ug/m**3	ug/m**2/s		
4 = ng/m**3	ng/m**2/s		
5 = Odour Units			

Visibility: extinction expressed in 1/Mega-meters (IPRTU is ignored)

Averaging time(s) reported  
-----

1-hr averages (L1HR) -- Default: T ! L1HR = T !

3-hr averages (L3HR) -- Default: T ! L3HR = T !

24-hr averages (L24HR) -- Default: T ! L24HR = T !

Run-length averages (LRUNL) -- Default: T ! LRUNL = T !

User-specified averaging time in hours - results for  
an averaging time of NAVG hours are reported for  
NAVG greater than 0:

(NAVG) -- Default: 0 ! NAVG = 8 !

Types of tabulations reported  
-----

1) Visibility: daily visibility tabulations are always reported  
for the selected receptors when ASPEC = VISIB.  
In addition, any of the other tabulations listed  
below may be chosen to characterize the light  
extinction coefficients.  
[List file or Plot/Analysis File]

2) Top 50 table for each averaging time selected  
[List file only]

(LT50) -- Default: T ! LT50 = T !

3) Top 'N' table for each averaging time selected  
[List file or Plot file]

(LTOPN) -- Default: F ! LTOPN = T !

-- Number of 'Top-N' values at each receptor  
selected (NTOP must be <= 4)

(NTOP) -- Default: 4 ! NTOP = 2 !

-- Specific ranks of 'Top-N' values reported  
(NTOP values must be entered)

(ITOP(4) array) -- Default: ! ITOP = 1, 2 !  
1,2,3,4

4) Threshold exceedance counts for each receptor and each averaging  
time selected  
[List file or Plot file]

(LEXCD) -- Default: F ! LEXCD = F !

-- Identify the threshold for each averaging time by assigning a non-negative value (output units).

-- Default: -1.0

Threshold for 1-hr averages (THRESH1) ! THRESH1 = -1.0 !  
 Threshold for 3-hr averages (THRESH3) ! THRESH3 = -1.0 !  
 Threshold for 24-hr averages (THRESH24) ! THRESH24 = -1.0 !  
 Threshold for NAVG-hr averages (THRESHN) ! THRESHN = -1.0 !

-- Counts for the shortest averaging period selected can be tallied daily, and receptors that experience more than NCOUNT counts over any NDAY period will be reported. This type of exceedance violation output is triggered only if NDAY > 0.

Accumulation period(Days)  
 (NDAY) -- Default: 0 ! NDAY = 0 !  
 Number of exceedances allowed  
 (NCOUNT) -- Default: 1 ! NCOUNT = 1 !

#### 5) Selected day table(s)

Echo Option -- Many records are written each averaging period selected and output is grouped by day  
 [List file or Plot file]

(LECHO) -- Default: F ! LECHO = F !

Timeseries Option -- Averages at all selected receptors for each selected averaging period are written to timeseries files. Each file contains one averaging period, and all receptors are written to a single record each averaging time.  
 [TSttUUUU.DAT files]

(LTIME) -- Default: F ! LTIME = F !

-- Days selected for output  
 (IECHO(366)) -- Default: 366\*0  
 ! IECHO = 366\*0 !  
 (366 values must be entered)

#### Plot output options

Plot files can be created for the Top-N, Exceedance, and Echo tables selected above. Two formats for these files are available, DATA and GRID. In the DATA format, results at all receptors are listed along with the receptor location [x,y,val1,val2,...]. In the GRID format, results at only gridded receptors are written, using a compact representation. The gridded values are written in rows (x varies), starting with the most southern row of the grid. The GRID format is given the .GRD extension, and includes headers compatible with the SURFER(R) plotting software.

A plotting and analysis file can also be created for the daily peak visibility summary output, in DATA format only.

Generate Plot file output in addition to writing tables to List file?

(LPLT) -- Default: F ! LPLT = F !

Use GRID format rather than DATA format, when available?

(LGRD) -- Default: F ! LGRD = F !

#### Additional Debug Output

Output selected information to List file for debugging?

(LDEBUG) -- Default: F ! LDEBUG = F !

!END!

\*\*\*\*\*
CALPOST Version 5.2 Level 991104
\*\*\*\*\*

Run Title:
DECKER FT MEADE AQRV IMPACTS AT CHASSAHOWITZKA NWA, SO2 4/24/00
RECEPTORS AT CHASSAHOWITZKA NWA, ALL AVERAGING ITMES, CALPOST
3 SIMPLE-CYCLE CTS, FUEL OIL, BASE LOAD, 32 DEGREES

INPUT GROUP: 1 -- General run control parameters

Option to run all periods found
in the met. file(s) (METRUN) Default: 0 ! METRUN = 0 !

METRUN = 0 - Run period explicitly defined below
METRUN = 1 - Run all periods in CALPUFF data file(s)

Starting date: Year (ISYR) -- No default ! ISYR = 1990 !
(used only if Month (ISMO) -- No default ! ISMO = 1 !
METRUN = 0) Day (ISDY) -- No default ! ISDY = 6 !
Hour (ISHR) -- No default ! ISHR = 0 !

Number of hours to process (NHRS) -- No default ! NHRS = 8616 !

Process every hour of data?(NREP) -- Default: 1 ! NREP = 1 !
(1 = every hour processed,
2 = every 2nd hour processed,
5 = every 5th hour processed, etc.)

Species & Concentration/Deposition Information

Species to process (ASPEC) -- No default ! ASPEC = SO2 !
(ASPEC = VISIB for visibility processing)

Layer/deposition code (ILAYER) -- Default: 1 ! ILAYER = 1 !
'1' for CALPUFF concentrations,
'-1' for dry deposition fluxes,
'-2' for wet deposition fluxes,
'-3' for wet+dry deposition fluxes.

Scaling factors of the form: -- Defaults: ! A = 0.0 !
X(new) = X(old) \* A + B A = 0.0 ! B = 0.0 !
(NOT applied if A = B = 0.0) B = 0.0

Add Hourly Background Concentrations/Fluxes?
(LBACK) -- Default: F ! LBACK = F !

Receptor information

Gridded receptors processed? (LG) -- Default: F ! LG = F !
Discrete receptors processed? (LD) -- Default: F ! LD = T !
CTS G Complex terrain receptors processed?
(LCT) -- Default: F ! LCT = F !

--Select range of DISCRETE receptors (only used when LD = T):

Select ALL DISCRETE receptors by setting NDRECP flag to -1;
OR
Select SPECIFIC DISCRETE receptors by entering a flag (0,1) for each
0 = discrete receptor not processed
1 = discrete receptor processed
using repeated value notation to select blocks of receptors:
23\*1, 15\*0, 12\*1
Flag for all receptors after the last one assigned is set to 0
(NDRECP) -- Default: -1

! NDRECP = -1 !

--Select range of GRIDDED receptors (only used when LG = T):



X index of LL corner (IBGRID) -- Default: -1 ! IBGRID = -1 !  
 (-1 OR 1 <= IBGRID <= NX)

Y index of LL corner (JBGRID) -- Default: -1 ! JBGRID = -1 !  
 (-1 OR 1 <= JBGRID <= NY)

X index of UR corner (IEGRID) -- Default: -1 ! IEGRID = -1 !  
 (-1 OR 1 <= IEGRID <= NX)

Y index of UR corner (JEGRID) -- Default: -1 ! JEGRID = -1 !  
 (-1 OR 1 <= JEGRID <= NY)

Note: Entire grid is processed if IBGRID=JBGRID=IEGRID=JEGRID=-1

--Specific gridded receptors can also be excluded from CALPOST processing by filling a processing grid array with 0s and 1s. If the processing flag for receptor index (i,j) is 1 (ON), that receptor will be processed if it lies within the range delineated by IBGRID, JBGRID, IEGRID, JEGRID and if LG=T. If it is 0 (OFF), it will not be processed in the run. By default, all array values are set to 1 (ON).

Number of gridded receptor rows provided in Subgroup (1a) to identify specific gridded receptors to process  
 (NGONOFF) -- Default: 0 ! NGONOFF = 0 !

!END!

-----  
 Subgroup (1a) -- Specific gridded receptors included/excluded  
 -----

Specific gridded receptors are excluded from CALPOST processing by filling a processing grid array with 0s and 1s. A total of NGONOFF lines are read here. Each line corresponds to one 'row' in the sampling grid, starting with the NORTHERNMOST row that contains receptors that you wish to exclude, and finishing with row 1 to the SOUTH (no intervening rows may be skipped). Within a row, each receptor position is assigned either a 0 or 1, starting with the westernmost receptor.

0 = gridded receptor not processed  
 1 = gridded receptor processed

Repeated value notation may be used to select blocks of receptors:  
 23\*1, 15\*0, 12\*1

Because all values are initially set to 1, any receptors north of the first row entered, or east of the last value provided in a row, remain ON.

(NGXRECP) -- Default: 1

-----  
 INPUT GROUP: 2 -- Visibility Parameters (ASPEC = VISIB)  
 -----

Maximum relative humidity (%) used in particle growth curve  
 (RHMAX) -- Default: 98 ! RHMAX = 0.0 !

Modeled species to be included in computing the light extinction

Include SULFATE?	(LVSO4)	-- Default: T	! LVSO4 = T !
Include NITRATE?	(LVNO3)	-- Default: T	! LVNO3 = T !
Include ORGANIC CARBON?	(LVOC)	-- Default: T	! LVOC = T !
Include COARSE PARTICLES?	(LVPMC)	-- Default: T	! LVPMC = T !
Include FINE PARTICLES?	(LVPMF)	-- Default: T	! LVPMF = T !

And, when ranking for TOP-N, TOP-50, and Exceedance tables,  
 Include BACKGROUND? (LVBK) -- Default: T ! LVBK = T !

Species name used for particulates in MODEL.DAT file

COARSE	(SPECPMC)	-- Default: PMC	! SPECPMC = PMC !
FINE	(SPECPMF)	-- Default: PMF	! SPECPMF = PMF !

Extinction Efficiency (1/Mm per ug/m\*\*3)

-----

MODELED particulate species:

PM COARSE (EPPMC) -- Default: 0.6 ! EPPMC = 0.6 !  
 PM FINE (EPPMF) -- Default: 1.0 ! EPPMF = 1.0 !

BACKGROUND particulate species:

PM COARSE (EPPMCBK) -- Default: 0.6 ! EPPMCBK = 0.6 !

Other species:

AMMONIUM SULFATE (EESO4) -- Default: 3.0 ! EESO4 = 3.0 !  
 AMMONIUM NITRATE (EENO3) -- Default: 3.0 ! EENO3 = 3.0 !  
 ORGANIC CARBON (EEOC) -- Default: 4.0 ! EEOC = 4.0 !  
 SOIL (EESOIL) -- Default: 1.0 ! EESOIL = 1.0 !  
 ELEMENTAL CARBON (EEEC) -- Default: 10. ! EEEC = 10.0 !

Background Extinction Computation

-----

Method used for background light extinction

(MVISBK) -- Default: 6 ! MVISBK = 2 !

- 1 = Supply single light extinction and hygroscopic fraction
  - IWAQM (1993) RH adjustment applied to hygroscopic background and modeled sulfate and nitrate
- 2 = Compute extinction from speciated PM measurements (A)
  - Hourly RH adjustment applied to observed and modeled sulfate and nitrate
  - RH factor is capped at RHMAX
- 3 = Compute extinction from speciated PM measurements (B)
  - Hourly RH adjustment applied to observed and modeled sulfate and nitrate
  - Receptor-hour excluded if RH>RHMAX
  - Receptor-day excluded if fewer than 6 valid receptor-hours
- 4 = Read hourly transmissometer background extinction measurements
  - Hourly RH adjustment applied to modeled sulfate and nitrate
  - Hour excluded if measurement invalid (missing, interference, or large RH)
  - Receptor-hour excluded if RH>RHMAX
  - Receptor-day excluded if fewer than 6 valid receptor-hours
- 5 = Read hourly nephelometer background extinction measurements
  - Rayleigh extinction value (BEXTRAY) added to measurement
  - Hourly RH adjustment applied to modeled sulfate and nitrate
  - Hour excluded if measurement invalid (missing, interference, or large RH)
  - Receptor-hour excluded if RH>RHMAX
  - Receptor-day excluded if fewer than 6 valid receptor-hours
- 6 = Compute extinction from speciated PM measurements
  - FLAG RH adjustment factor applied to observed and modeled sulfate and nitrate

Additional inputs used for MVISBK = 1:

-----

Background light extinction (1/Mm)

(BEXTBK) -- No default ! BEXTBK = 0.0 !

Percentage of particles affected by relative humidity

(RHFRAC) -- No default ! RHFRAC = 0.0 !

Additional inputs used for MVISBK = 6:

-----

Extinction coefficients for hygroscopic species (modeled and background) are computed using a monthly RH adjustment factor in place of an hourly RH factor (VISB.DAT file is NOT needed). Enter the 12 monthly factors here (RHFAC). Month 1 is January.

(RHFAC) -- No default ! RHFAC = 0.0, 0.0, 0.0, 0.0,  
 0.0, 0.0, 0.0, 0.0,  
 0.0, 0.0, 0.0, 0.0 !

Additional inputs used for MVISBK = 2,3,6:

-----

Background extinction coefficients are computed from monthly CONCENTRATIONS of ammonium sulfate (BKS04), ammonium nitrate (BKN03), coarse particulates (BKPMC), organic carbon (BKOC), soil (BKSOIL), and elemental carbon (BKEC). Month 1 is January. (ug/m\*\*3)

(BKS04) -- No default ! BKS04 = 0.0, 0.0, 0.0, 0.0,  
 0.0, 0.0, 0.0, 0.0,

```

          0.0, 0.0, 0.0, 0.0 !
(BKNO3) -- No default ! BKNO3 = 0.0, 0.0, 0.0, 0.0,
          0.0, 0.0, 0.0, 0.0,
          0.0, 0.0, 0.0, 0.0 !
(BKPMC) -- No default ! BKPMC = 0.0, 0.0, 0.0, 0.0,
          0.0, 0.0, 0.0, 0.0,
          0.0, 0.0, 0.0, 0.0 !
(BKOC)  -- No default ! BKOC  = 0.0, 0.0, 0.0, 0.0,
          0.0, 0.0, 0.0, 0.0,
          0.0, 0.0, 0.0, 0.0 !
(BKSOIL) -- No default ! BKSOIL= 0.0, 0.0, 0.0, 0.0,
          0.0, 0.0, 0.0, 0.0,
          0.0, 0.0, 0.0, 0.0 !
(BKEC)  -- No default ! BKEC  = 0.0, 0.0, 0.0, 0.0,
          0.0, 0.0, 0.0, 0.0,
          0.0, 0.0, 0.0, 0.0 !

```

Additional inputs used for MVISBK = 2,3,5,6:

```

-----
Extinction due to Rayleigh scattering is added (1/Mm)
(BEXTRAY) -- Default: 10.0 ! BEXTRAY = 0.0 !

```

!END!

-----

INPUT GROUP: 3 -- Output options

-----

#### Output Units

```

-----
Units for All Output      (IPRTU) -- Default: 1 ! IPRTU = 3 !
      for                  for
      Concentration      Deposition
1 =      g/m**3          g/m**2/s
2 =      mg/m**3         mg/m**2/s
3 =      ug/m**3         ug/m**2/s
4 =      ng/m**3         ng/m**2/s
5 =      Odour Units

```

Visibility: extinction expressed in 1/Mega-meters (IPRTU is ignored)

#### Averaging time(s) reported

```

-----
1-hr averages      (L1HR) -- Default: T ! L1HR = T !
3-hr averages      (L3HR) -- Default: T ! L3HR = T !
24-hr averages     (L24HR) -- Default: T ! L24HR = T !
Run-length averages (LRUNL) -- Default: T ! LRUNL = T !

User-specified averaging time in hours - results for
an averaging time of NAVG hours are reported for
NAVG greater than 0:
      (NAVG) -- Default: 0 ! NAVG = 8 !

```

#### Types of tabulations reported

- 
- 1) Visibility: daily visibility tabulations are always reported for the selected receptors when ASPEC = VISIB. In addition, any of the other tabulations listed below may be chosen to characterize the light extinction coefficients.  
[List file or Plot/Analysis File]
  - 2) Top 50 table for each averaging time selected  
[List file only]  
(LT50) -- Default: T ! LT50 = T !
  - 3) Top 'N' table for each averaging time selected  
[List file or Plot file]  
(LTOPN) -- Default: F ! LTOPN = T !

```
-- Number of 'Top-N' values at each receptor
selected (NTOP must be <= 4)
      (NTOP) -- Default: 4 ! NTOP = 2 !

-- Specific ranks of 'Top-N' values reported
(NTOP values must be entered)
      (ITOP(4) array) -- Default: ! ITOP = 1, 2 !
                          1,2,3,4
```

4) Threshold exceedance counts for each receptor and each averaging time selected  
[List file or Plot file]

```
(LEXCD) -- Default: F ! LEXCD = F !
```

```
-- Identify the threshold for each averaging time by assigning a
non-negative value (output units).
```

```
-- Default: -1.0
```

```
Threshold for 1-hr averages (THRESH1) ! THRESH1 = -1.0 !
```

```
Threshold for 3-hr averages (THRESH3) ! THRESH3 = -1.0 !
```

```
Threshold for 24-hr averages (THRESH24) ! THRESH24 = -1.0 !
```

```
Threshold for NAVG-hr averages (THRESHN) ! THRESHN = -1.0 !
```

```
-- Counts for the shortest averaging period selected can be
tallied daily, and receptors that experience more than NCOUNT
counts over any NDAY period will be reported. This type of
exceedance violation output is triggered only if NDAY > 0.
```

```
Accumulation period(Days)
```

```
(NDAY) -- Default: 0 ! NDAY = 0 !
```

```
Number of exceedances allowed
```

```
(NCOUNT) -- Default: 1 ! NCOUNT = 1 !
```

5) Selected day table(s)

```
Echo Option -- Many records are written each averaging period
selected and output is grouped by day
```

```
[List file or Plot file]
```

```
(LECHO) -- Default: F ! LECHO = F !
```

```
Timeseries Option -- Averages at all selected receptors for
each selected averaging period are written to timeseries files.
Each file contains one averaging period, and all receptors are
written to a single record each averaging time.
```

```
[TSttUUUU.DAT files]
```

```
(LTIME) -- Default: F ! LTIME = F !
```

```
-- Days selected for output
```

```
(IECHO(366)) -- Default: 366*0
```

```
! IECHO = 366*0 !
```

```
(366 values must be entered)
```

Plot output options

```
-----
Plot files can be created for the Top-N, Exceedance, and Echo
tables selected above. Two formats for these files are available,
DATA and GRID. In the DATA format, results at all receptors are
listed along with the receptor location [x,y,val1,val2,...].
In the GRID format, results at only gridded receptors are written,
using a compact representation. The gridded values are written in
rows (x varies), starting with the most southern row of the grid.
The GRID format is given the .GRD extension, and includes headers
compatible with the SURFER(R) plotting software.
```

```
A plotting and analysis file can also be created for the daily
peak visibility summary output, in DATA format only.
```

```
Generate Plot file output in addition to writing tables
to List file?
```

```
(LPLT) -- Default: F ! LPLT = F !
```

```
Use GRID format rather than DATA format,
```

when available?

(LGRD) -- Default: F ! LGRD = F !

Additional Debug Output

-----

Output selected information to List file  
for debugging?

(LDEBUG) -- Default: F ! LDEBUG = F !

!END!

-----  
NOTICE: Starting year in control file sets the  
expected century for the simulation. All  
YY years are converted to YYYY years in  
the range: 1940 2039  
-----

\*\*\*\*\*  
CALPOST Version 5.2 Level 991104  
\*\*\*\*\*

CALPOST Control File Input Summary -----

Replace run data with data in Puff file 1=Y: 0  
Run starting date -- year: 1990  
month: 1  
day: 5  
Julian day: 5  
Time at beginning of run - hour(0-23): 23  
- second: 0  
Run length (hours): 8616

Every hour of data processed -- NREP = 1

Species & Concentration/Deposition Information

Species: SO2  
Layer of processed data: 1  
(>0=conc, -1=dry flux, -2=wet flux, -3=wet & dry flux)  
Multiplicative scaling factor: 0.0000E+00  
Additive scaling factor: 0.0000E+00  
Hourly background values used?: F

Receptor information

Gridded receptors processed?: F  
Discrete receptors processed?: T  
CTSG Complex terrain receptors processed?: F

Discrete Receptors Processed

(All Discrete Receptors are Used)

Visibility Processing is NOT Selected

Output options

Units requested for output: (ug/m\*\*3)

Averaging time(s) selected

User-specified averaging time (NAVG hours): 8  
1-hr averages: T  
3-hr averages: T  
24-hr averages: T  
NAVG-hr averages: T  
Length of run averages: T

Output components selected

Top-50: T  
 Top-N values at each receptor: T  
 Exceedance counts at each receptor: F  
 Output selected information for debugging: F  
 Echo tables for selected days: F  
 Time-series for selected days: F

Top "n" table control

Number of "top" values at each receptor: 2  
 Specific ranks of "top" values reported: 1 2

Plot file option

Plot files created: F

IDENTIFICATION OF PROCESSED MODEL FILE -----

CALPUFF 5.2 991104a

REFINED SIGNIFICANT IMPACT ANALYSIS, CALPUFF, DECKER FT MEADE 3 S-C CTS 4/24/00  
 RECEPTORS AT CHASSAHOWITZKA NWA, PLANT ONLY, NATURAL GAS FUEL  
 FDEP CHASSAHOWITZKA CALMET DOMAIN WITH PRECIPITATION, NAT. GAS, BASE/32 DEG

Averaging time for values reported from model:  
 1 HOUR

Number of averaging periods in file from model:  
 8616

Chemical species names for each layer in model:

SO2 1  
 SO4 1  
 NOX 1  
 HNO3 1  
 NO3 1  
 PM10 1  
 CO 1

\*\*\*\*\* NOTICE \*\*\*\*\*  
 NDRECP array reset to full range: all 1s

-----  
INPUT FILES

Default Name	Unit No.	File Name and Path
CALPOST.INP	5	calpost.inp
MODEL.DAT	4	calpuff.con

-----  
OUTPUT FILES

Default Name	Unit No.	File Name and Path
CALPOST.LST	8	calpost.lst

\*\*\*\*\*  
 CALPOST Version 5.2 Level 991104  
 \*\*\*\*\*

S02 1

TOP-50 1 HOUR AVERAGE CONCENTRATION VALUES (ug/m\*\*3)

YEAR	DAY	TIME(HHMM)	RECEPTOR	TYPE	CONCENTRATION	COORDINATES (km)
1990	88	0900	( 0, 6)	D	6.1812E-01	343.000 3176.200
1990	88	0900	( 0, 7)	D	6.0870E-01	343.700 3178.300



1990	20	0800	( 0, 4)	D	2.9894E-01	340.700	3171.900
1990	20	0800	( 0, 5)	D	2.9540E-01	342.000	3174.000
1990	89	0500	( 0, 9)	D	2.9195E-01	341.100	3183.400
1990	291	1100	( 0, 2)	D	2.9124E-01	340.300	3167.700
1990	89	0500	( 0, 7)	D	2.9114E-01	343.700	3178.300
1990	89	0500	( 0, 8)	D	2.9112E-01	342.400	3180.600
1990	20	0800	( 0, 3)	D	2.8907E-01	340.300	3169.800
1990	88	1100	( 0, 2)	D	2.8698E-01	340.300	3167.700
1990	332	0800	( 0, 1)	D	2.8598E-01	340.300	3165.700
1990	136	1100	( 0, 4)	D	2.8524E-01	340.700	3171.900
1990	332	0800	( 0, 2)	D	2.8455E-01	340.300	3167.700
1990	136	1100	( 0, 13)	D	2.8158E-01	331.500	3183.400
1990	123	1100	( 0, 3)	D	2.8128E-01	340.300	3169.800
1990	332	0800	( 0, 3)	D	2.7817E-01	340.300	3169.800
1990	20	0800	( 0, 12)	D	2.7572E-01	334.000	3183.400
1990	20	0800	( 0, 13)	D	2.7477E-01	331.500	3183.400
1990	20	0800	( 0, 6)	D	2.7330E-01	343.000	3176.200
1990	20	0800	( 0, 2)	D	2.7290E-01	340.300	3167.700
1990	20	1100	( 0, 6)	D	2.7107E-01	343.000	3176.200
1990	192	1100	( 0, 1)	D	2.6961E-01	340.300	3165.700
1990	228	1100	( 0, 1)	D	2.6859E-01	340.300	3165.700
1990	20	1100	( 0, 7)	D	2.6757E-01	343.700	3178.300
1990	332	0800	( 0, 13)	D	2.6568E-01	331.500	3183.400
1990	354	1400	( 0, 1)	D	2.6564E-01	340.300	3165.700
1990	20	0800	( 0, 11)	D	2.6559E-01	336.500	3183.400
1990	332	0800	( 0, 4)	D	2.6547E-01	340.700	3171.900
1990	89	0500	( 0, 10)	D	2.6390E-01	339.000	3183.400
1990	291	1100	( 0, 3)	D	2.6302E-01	340.300	3169.800
1990	88	0800	( 0, 4)	D	2.6249E-01	340.700	3171.900
1990	89	0500	( 0, 6)	D	2.6209E-01	343.000	3176.200
1990	20	1100	( 0, 5)	D	2.6178E-01	342.000	3174.000
1990	88	0800	( 0, 3)	D	2.6146E-01	340.300	3169.800
1990	136	0800	( 0, 1)	D	2.6076E-01	340.300	3165.700

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 CALPOST Version 5.2 Level 991104  
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SO2 1

TOP-50 24 HOUR AVERAGE CONCENTRATION VALUES (ug/m\*\*3)

YEAR	DAY	TIME(HHMM)	RECEPTOR	TYPE	CONCENTRATION	COORDINATES (km)
1990	136	2300	( 0, 1)	D	1.2422E-01	340.300 3165.700
1990	136	2300	( 0, 2)	D	1.1828E-01	340.300 3167.700
1990	136	2300	( 0, 3)	D	1.1070E-01	340.300 3169.800
1990	228	2300	( 0, 1)	D	1.0126E-01	340.300 3165.700
1990	136	2300	( 0, 4)	D	1.0096E-01	340.700 3171.900
1990	228	2300	( 0, 2)	D	9.9755E-02	340.300 3167.700
1990	88	2300	( 0, 6)	D	9.9522E-02	343.000 3176.200
1990	20	2300	( 0, 6)	D	9.9303E-02	343.000 3176.200
1990	20	2300	( 0, 5)	D	9.9301E-02	342.000 3174.000
1990	88	2300	( 0, 7)	D	9.9017E-02	343.700 3178.300
1990	228	2300	( 0, 3)	D	9.7619E-02	340.300 3169.800
1990	136	2300	( 0, 13)	D	9.6825E-02	331.500 3183.400
1990	88	2300	( 0, 5)	D	9.6760E-02	342.000 3174.000
1990	20	2300	( 0, 7)	D	9.6304E-02	343.700 3178.300
1990	88	2300	( 0, 8)	D	9.6285E-02	342.400 3180.600
1990	228	2300	( 0, 4)	D	9.6004E-02	340.700 3171.900
1990	228	2300	( 0, 5)	D	9.5338E-02	342.000 3174.000
1990	20	2300	( 0, 4)	D	9.4548E-02	340.700 3171.900
1990	20	2300	( 0, 8)	D	9.4439E-02	342.400 3180.600
1990	228	2300	( 0, 6)	D	9.3667E-02	343.000 3176.200
1990	123	2300	( 0, 1)	D	9.3490E-02	340.300 3165.700
1990	20	2300	( 0, 10)	D	9.3334E-02	339.000 3183.400
1990	88	2300	( 0, 9)	D	9.2803E-02	341.100 3183.400
1990	20	2300	( 0, 11)	D	9.2404E-02	336.500 3183.400
1990	88	2300	( 0, 10)	D	9.1883E-02	339.000 3183.400
1990	20	2300	( 0, 9)	D	9.1702E-02	341.100 3183.400
1990	228	2300	( 0, 7)	D	9.1400E-02	343.700 3178.300
1990	88	2300	( 0, 4)	D	9.0103E-02	340.700 3171.900
1990	20	2300	( 0, 3)	D	8.9371E-02	340.300 3169.800
1990	136	2300	( 0, 12)	D	8.9014E-02	334.000 3183.400
1990	88	2300	( 0, 11)	D	8.8887E-02	336.500 3183.400
1990	20	2300	( 0, 12)	D	8.8605E-02	334.000 3183.400



1990	136	2300	( 0, 5)	D	8.6936E-02	342.000	3174.000
1990	192	2300	( 0, 1)	D	8.6459E-02	340.300	3165.700
1990	228	2300	( 0, 8)	D	8.6177E-02	342.400	3180.600
1990	88	2300	( 0, 12)	D	8.5194E-02	334.000	3183.400
1990	291	2300	( 0, 1)	D	8.4205E-02	340.300	3165.700
1990	20	2300	( 0, 2)	D	8.4010E-02	340.300	3167.700
1990	88	2300	( 0, 3)	D	8.3645E-02	340.300	3169.800
1990	291	2300	( 0, 2)	D	8.2629E-02	340.300	3167.700
1990	20	2300	( 0, 13)	D	8.2407E-02	331.500	3183.400
1990	123	2300	( 0, 2)	D	8.2174E-02	340.300	3167.700
1990	192	2300	( 0, 2)	D	8.2058E-02	340.300	3167.700
1990	89	2300	( 0, 7)	D	8.0864E-02	343.700	3178.300
1990	228	2300	( 0, 9)	D	8.0618E-02	341.100	3183.400
1990	88	2300	( 0, 13)	D	7.9837E-02	331.500	3183.400
1990	136	2300	( 0, 11)	D	7.9668E-02	336.500	3183.400
1990	291	2300	( 0, 3)	D	7.9633E-02	340.300	3169.800
1990	89	2300	( 0, 8)	D	7.9388E-02	342.400	3180.600
1990	228	2300	( 0, 10)	D	7.8203E-02	339.000	3183.400

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 CALPOST Version 5.2 Level 991104  
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SO2 1

TOP-50 8 HOUR AVERAGE CONCENTRATION VALUES (ug/m\*\*3)

YEAR	DAY	TIME(HHMM)	RECEPTOR	TYPE	CONCENTRATION	COORDINATES (km)	
1990	136	1500	( 0, 1)	D	2.6222E-01	340.300	3165.700
1990	136	1500	( 0, 2)	D	2.5355E-01	340.300	3167.700
1990	88	1500	( 0, 7)	D	2.4988E-01	343.700	3178.300
1990	88	1500	( 0, 8)	D	2.4529E-01	342.400	3180.600
1990	88	1500	( 0, 6)	D	2.4509E-01	343.000	3176.200
1990	123	1500	( 0, 1)	D	2.4154E-01	340.300	3165.700
1990	136	1500	( 0, 3)	D	2.3957E-01	340.300	3169.800
1990	88	1500	( 0, 9)	D	2.3919E-01	341.100	3183.400
1990	88	1500	( 0, 10)	D	2.3397E-01	339.000	3183.400
1990	88	1500	( 0, 5)	D	2.3024E-01	342.000	3174.000
1990	291	1500	( 0, 1)	D	2.2365E-01	340.300	3165.700
1990	88	1500	( 0, 11)	D	2.2264E-01	336.500	3183.400
1990	136	1500	( 0, 4)	D	2.2018E-01	340.700	3171.900
1990	20	1500	( 0, 7)	D	2.1894E-01	343.700	3178.300
1990	291	1500	( 0, 2)	D	2.1832E-01	340.300	3167.700
1990	20	1500	( 0, 6)	D	2.1654E-01	343.000	3176.200
1990	20	1500	( 0, 8)	D	2.1632E-01	342.400	3180.600
1990	123	1500	( 0, 2)	D	2.1499E-01	340.300	3167.700
1990	20	1500	( 0, 9)	D	2.1289E-01	341.100	3183.400
1990	20	1500	( 0, 10)	D	2.0987E-01	339.000	3183.400
1990	88	1500	( 0, 12)	D	2.0977E-01	334.000	3183.400
1990	136	1500	( 0, 13)	D	2.0930E-01	331.500	3183.400
1990	291	1500	( 0, 3)	D	2.0873E-01	340.300	3169.800
1990	228	1500	( 0, 1)	D	2.0602E-01	340.300	3165.700
1990	88	1500	( 0, 4)	D	2.0468E-01	340.700	3171.900
1990	20	1500	( 0, 5)	D	2.0434E-01	342.000	3174.000
1990	192	1500	( 0, 1)	D	2.0083E-01	340.300	3165.700
1990	228	1500	( 0, 2)	D	2.0003E-01	340.300	3167.700
1990	20	1500	( 0, 11)	D	1.9872E-01	336.500	3183.400
1990	291	1500	( 0, 4)	D	1.9767E-01	340.700	3171.900
1990	226	1500	( 0, 5)	D	1.9338E-01	342.000	3174.000
1990	88	1500	( 0, 13)	D	1.9256E-01	331.500	3183.400
1990	228	1500	( 0, 3)	D	1.9251E-01	340.300	3169.800
1990	136	1500	( 0, 12)	D	1.9248E-01	334.000	3183.400
1990	226	1500	( 0, 6)	D	1.9222E-01	343.000	3176.200
1990	136	1500	( 0, 5)	D	1.9095E-01	342.000	3174.000
1990	192	1500	( 0, 2)	D	1.8908E-01	340.300	3167.700
1990	226	1500	( 0, 4)	D	1.8890E-01	340.700	3171.900
1990	226	1500	( 0, 12)	D	1.8789E-01	334.000	3183.400
1990	226	1500	( 0, 8)	D	1.8727E-01	342.400	3180.600
1990	89	0700	( 0, 7)	D	1.8717E-01	343.700	3178.300
1990	228	1500	( 0, 4)	D	1.8648E-01	340.700	3171.900
1990	226	1500	( 0, 7)	D	1.8646E-01	343.700	3178.300
1990	226	1500	( 0, 11)	D	1.8601E-01	336.500	3183.400
1990	123	1500	( 0, 3)	D	1.8590E-01	340.300	3169.800
1990	226	1500	( 0, 13)	D	1.8582E-01	331.500	3183.400
1990	89	0700	( 0, 8)	D	1.8450E-01	342.400	3180.600



2	340.300	3167.700	5.0880E-01 (1990,136,0900)	4.1934E-01 (1990,332,0700)
3	340.300	3169.800	4.7731E-01 (1990,088,0900)	4.6303E-01 (1990,136,0900)
4	340.700	3171.900	5.4172E-01 (1990,088,0900)	4.0911E-01 (1990,088,0800)
5	342.000	3174.000	5.9750E-01 (1990,088,0900)	4.3198E-01 (1990,088,1000)
6	343.000	3176.200	6.1812E-01 (1990,088,0900)	4.5178E-01 (1990,088,1000)
7	343.700	3178.300	6.0870E-01 (1990,088,0900)	4.5136E-01 (1990,088,1000)
8	342.400	3180.600	5.7989E-01 (1990,088,0900)	4.4157E-01 (1990,088,1000)
9	341.100	3183.400	5.4057E-01 (1990,088,0900)	4.2577E-01 (1990,088,1000)
10	339.000	3183.400	5.3741E-01 (1990,088,0900)	4.2569E-01 (1990,088,1000)
11	336.500	3183.400	5.1904E-01 (1990,088,0900)	4.1249E-01 (1990,088,1000)
12	334.000	3183.400	4.8703E-01 (1990,088,0900)	4.1107E-01 (1990,088,1000)
13	331.500	3183.400	4.4772E-01 (1990,088,0900)	3.8979E-01 (1990,088,1000)

\*\*\*\*\*  
 CALPOST Version 5.2 Level 991104  
 \*\*\*\*\*

SO2 1

2 RANKED 3 HOUR AVERAGE CONCENTRATION VALUES AT EACH DISCRETE RECEPTOR (YEAR,DAY,ENDING TIME) (ug/m\*\*3)

RECEPTOR	COORDINATES (km)		1 RANK	2 RANK
1	340.300	3165.700	3.6020E-01 (1990,123,1100)	3.4330E-01 (1990,136,1100)
2	340.300	3167.700	3.3533E-01 (1990,136,1100)	3.2348E-01 (1990,123,1100)
3	340.300	3169.800	3.3215E-01 (1990,088,1100)	3.1553E-01 (1990,136,1100)
4	340.700	3171.900	3.7909E-01 (1990,088,1100)	2.9894E-01 (1990,020,0800)
5	342.000	3174.000	4.2781E-01 (1990,088,1100)	2.9540E-01 (1990,020,0800)
6	343.000	3176.200	4.5333E-01 (1990,088,1100)	2.7330E-01 (1990,020,0800)
7	343.700	3178.300	4.5741E-01 (1990,088,1100)	2.9114E-01 (1990,089,0500)
8	342.400	3180.600	4.4639E-01 (1990,088,1100)	2.9112E-01 (1990,089,0500)
9	341.100	3183.400	4.3069E-01 (1990,088,1100)	2.9195E-01 (1990,089,0500)
10	339.000	3183.400	4.2627E-01 (1990,088,1100)	2.6390E-01 (1990,089,0500)
11	336.500	3183.400	4.0957E-01 (1990,088,1100)	2.6559E-01 (1990,020,0800)
12	334.000	3183.400	3.9041E-01 (1990,088,1100)	2.7572E-01 (1990,020,0800)
13	331.500	3183.400	3.6082E-01 (1990,088,1100)	2.8158E-01 (1990,136,1100)

\*\*\*\*\*  
 CALPOST Version 5.2 Level 991104  
 \*\*\*\*\*

SO2 1

2 RANKED 24 HOUR AVERAGE CONCENTRATION VALUES AT EACH DISCRETE RECEPTOR (YEAR,DAY,ENDING TIME) (ug/m\*\*3)

RECEPTOR	COORDINATES (km)		1 RANK	2 RANK
1	340.300	3165.700	1.2422E-01 (1990,136,2300)	1.0126E-01 (1990,228,2300)
2	340.300	3167.700	1.1828E-01 (1990,136,2300)	9.9755E-02 (1990,228,2300)
3	340.300	3169.800	1.1070E-01 (1990,136,2300)	9.7619E-02 (1990,228,2300)
4	340.700	3171.900	1.0096E-01 (1990,136,2300)	9.6004E-02 (1990,228,2300)
5	342.000	3174.000	9.9301E-02 (1990,020,2300)	9.6760E-02 (1990,088,2300)
6	343.000	3176.200	9.9522E-02 (1990,088,2300)	9.9303E-02 (1990,020,2300)
7	343.700	3178.300	9.9017E-02 (1990,088,2300)	9.6304E-02 (1990,020,2300)
8	342.400	3180.600	9.6285E-02 (1990,088,2300)	9.4439E-02 (1990,020,2300)
9	341.100	3183.400	9.2803E-02 (1990,088,2300)	9.1702E-02 (1990,020,2300)
10	339.000	3183.400	9.3334E-02 (1990,020,2300)	9.1883E-02 (1990,088,2300)
11	336.500	3183.400	9.2404E-02 (1990,020,2300)	8.8887E-02 (1990,088,2300)
12	334.000	3183.400	8.9014E-02 (1990,136,2300)	8.8605E-02 (1990,020,2300)
13	331.500	3183.400	9.6825E-02 (1990,136,2300)	8.2407E-02 (1990,020,2300)

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 CALPOST Version 5.2 Level 991104  
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SO2 1

2 RANKED 8 HOUR AVERAGE CONCENTRATION VALUES AT EACH DISCRETE RECEPTOR (YEAR,DAY,ENDING TIME) (ug/m\*\*3)

RECEPTOR	COORDINATES (km)		1 RANK	2 RANK
1	340.300	3165.700	2.6222E-01 (1990,136,1500)	2.4154E-01 (1990,123,1500)
2	340.300	3167.700	2.5355E-01 (1990,136,1500)	2.1832E-01 (1990,291,1500)
3	340.300	3169.800	2.3957E-01 (1990,136,1500)	2.0873E-01 (1990,291,1500)
4	340.700	3171.900	2.2018E-01 (1990,136,1500)	2.0468E-01 (1990,088,1500)
5	342.000	3174.000	2.3024E-01 (1990,088,1500)	2.0434E-01 (1990,020,1500)
6	343.000	3176.200	2.4509E-01 (1990,088,1500)	2.1654E-01 (1990,020,1500)

7	343.700	3178.300	2.4988E-01	(1990,088,1500)	2.1894E-01	(1990,020,1500)
8	342.400	3180.600	2.4529E-01	(1990,088,1500)	2.1632E-01	(1990,020,1500)
9	341.100	3183.400	2.3919E-01	(1990,088,1500)	2.1289E-01	(1990,020,1500)
10	339.000	3183.400	2.3397E-01	(1990,088,1500)	2.0987E-01	(1990,020,1500)
11	336.500	3183.400	2.2264E-01	(1990,088,1500)	1.9872E-01	(1990,020,1500)
12	334.000	3183.400	2.0977E-01	(1990,088,1500)	1.9248E-01	(1990,136,1500)
13	331.500	3183.400	2.0930E-01	(1990,136,1500)	1.9256E-01	(1990,088,1500)

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 CALPOST Version 5.2 Level 991104  
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8616 HOUR AVERAGE CONCENTRATION AT EACH RECEPTOR FOR THE PERIOD ENDING YEAR: 1990 DAY: 364 HOUR(0-23): 23 SEC:

DISCRETE RECEPTORS: SO2 1

RECEPTOR	COORDINATES (km)		CONCENTRATION	RECEPTOR	COORDINATES (km)		CONCENTRATION
1	340.300	3165.700	6.7575E-03	7	343.700	3178.300	5.8447E-03
2	340.300	3167.700	6.5984E-03	8	342.400	3180.600	5.7071E-03
3	340.300	3169.800	6.4410E-03	9	341.100	3183.400	5.5456E-03
4	340.700	3171.900	6.2844E-03	10	339.000	3183.400	5.5388E-03
5	342.000	3174.000	6.1300E-03	11	336.500	3183.400	5.5213E-03
6	343.000	3176.200	5.9789E-03	12	334.000	3183.400	5.5033E-03
				13	331.500	3183.400	5.4756E-03

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SUMMARY SECTION

SO2 1

(ug/m\*\*3)

RECEPTOR	COORDINATES (km)		TYPE	PEAK (YEAR, DAY, ENDING TIME)	FOR RANK	FOR AVERAGE PERIOD
6	343.000	3176.200	DISCRETE	6.1812E-01 (1990,088,0900)	RANK 1	1 HOUR
3	340.300	3169.800	DISCRETE	4.6303E-01 (1990,136,0900)	RANK 2	1 HOUR
7	343.700	3178.300	DISCRETE	4.5741E-01 (1990,088,1100)	RANK 1	3 HOUR
1	340.300	3165.700	DISCRETE	3.4330E-01 (1990,136,1100)	RANK 2	3 HOUR
1	340.300	3165.700	DISCRETE	1.2422E-01 (1990,136,2300)	RANK 1	24 HOUR
1	340.300	3165.700	DISCRETE	1.0126E-01 (1990,228,2300)	RANK 2	24 HOUR
1	340.300	3165.700	DISCRETE	2.6222E-01 (1990,136,1500)	RANK 1	8 HOUR
1	340.300	3165.700	DISCRETE	2.4154E-01 (1990,123,1500)	RANK 2	8 HOUR
1	340.300	3165.700	DISCRETE	6.7575E-03	RANK 1	8616 HOUR