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Division of Air
Resources Management

ATTACHMENT 4

**DETAILED EMISSION CALCULATIONS
FOR THE COMBUSTION TURBINE**

Table A-1. Design Information and Stack Parameters for DESTEC Central Florida Cogeneration Facility-
GE PG7221(FA), Dry Low NOx II Combustion System, Distillate Oil, Base Load

Data	* Not Available *		* Not Available *			
	Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F		
A	B	C	D	E	F	G
General						
Power (kW)		183,700.0		159,200.0		142,500.0
Heat Rate (Btu/kwh)		10,070.0		10,320.0		10,650.0
CT Exhaust Flow						
Mass Flow (lb/hr)		3,743,000		3,390,000		3,189,000
Temperature (oF)		1,060		1,102		1,127
Moisture (% Vol.)		11.59		12.40		12.71
Oxygen (% Vol.)		10.96		10.95		11.03
Molecular Weight		28.25		28.15		28.10
Heat Input (MMBtu/hr)= Power (kW) x Heat Rate (Btu/kwh) ÷ 1,000,000 Btu/MMBtu						
Power (kW)		183,700.0		159,200.0		142,500.0
Heat Rate (Btu/kwh)		10,070.0		10,320.0		10,650.0
Heat Input (MMBtu/hr)		1,849.9		1,642.9		1,517.6
Fuel Oil Consumption (lb/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu ÷ Fuel Heat Content, LHV (Btu/lb)						
Heat Input (MMBtu/hr)		1,849.9		1,642.9		1,517.6
Heat Content, LHV (Btu/lb)		18,550		18,550		18,550
Fuel Oil (lb/hr)		99,722.9		88,568.4		81,812.7
Volume Flow (acfm)= [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F)+ 460°F)] ÷ [Molecular weight x 2116.8] ÷ 60 min/hr						
Mass Flow (lb/hr)		3,743,000		3,390,000		3,189,000
Temperature (°F)		1,060		1,102		1,127
Molecular Weight		28.25		28.15		28.10
Volume Flow (acfm)		2,450,287		2,288,314		2,190,589
Volume Flow (scfm)= [(Mass Flow (lb/hr) x 1,545 x (68°F + 460°F)] ÷ [Molecular weight x 2116.8] ÷ 60 min/hr						
Mass Flow (lb/hr)		3,743,000		3,390,000		3,189,000
Temperature (°F)		68		68		68
Molecular Weight		28.25		28.15		28.10
Volume Flow (scfm)		851,152		773,514		728,816
HRSR Stack Data						
Stack Height (ft)		180		180		180
Diameter (ft)		18.0		18.0		18.0
Volume Flow (acfm) from HRSR= [Volume flow (acfm) x (HRSR temp.(°F)+ 460°F)] ÷ [CT temp.(°F)+ 460°F]						
Volume Flow (acfm) from CT		2,450,287		2,288,314		2,190,589
CT Temperature (°F)		1,060		1,102		1,127
HRSR Temperature (°F)		205		205		205
Volume Flow (acfm) from HRSR		1,072,001		974,218		917,922
Velocity (ft/sec)= Volume flow (acfm) from HRSR ÷ [((diameter)²+ 4) x 3.14159] ÷ 60 sec/min						
Volume Flow (acfm) from HRSR		1,072,001		974,218		917,922
Diameter (ft)		18.0		18.0		18.0
Velocity (ft/sec)		70.2		63.8		60.1

Note: Universal gas constant= 1,545 ft-lb(force)/°R; atmospheric pressure= 2,116.8 lb(force)/ft²

Source: General Electric, 1992.

Table A-2. Maximum Emissions for Criteria Pollutants for DESTEC Central Florida Cogeneration Facility-
GE PG7221(FA), Dry Low NOx II Combustion System, Distillate Oil, Base Load

Pollutant	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F	
	Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F		
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Particulate (lb/hr)= Emission rate (lb/hr) from manufacturer						
Basis, lb/hr (manufactur.) (1)		17.0		17.0		17.0
lb/hr		17.0		17.0		17.0
TPY		2.6		2.6		2.6
Sulfur Dioxide (lb/hr)= Fuel oil (lb/hr) x sulfur content(fraction) x (lb SO2/lb S) x fraction emitted as SO2						
Fuel Oil (lb/hr)		99,722.9		88,568.4		81,812.7
Sulfur content (%)		0.05		0.05		0.05
lb SO2/lb S (64/32)		2.0		2.0		2.0
SO2 Fraction emitted		1.00		1.00		1.00
lb/hr		99.72		88.57		81.81
TPY		15.0		13.3		12.3
Nitrogen Oxides (lb/hr)= NOx(ppm) x [(20.9 x (1 - Moisture%)/100)] - Oxygen(%) x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		42.0		42.0		42.0
Moisture (%)		11.59		12.4		12.71
Oxygen (%)		10.96		10.95		11.03
Volume Flow (acfm)		2,450,287		2,288,314		2,190,589
Temperature (°F)		1060		1102		1127
lb/hr		326.2		290.2		268.0
TPY		48.9		43.5		40.2
Carbon Monoxide (lb/hr)= CO(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		30.0		30.0		30.0
Moisture (%)		11.59		12.4		12.71
Volume Flow (acfm)		2,450,287		2,288,314		2,190,589
Temperature (°F)		1060		1102		1127
lb/hr		98.4		88.6		83.2
TPY		14.8		13.3		12.5
VOCs (lb/hr)= VOC(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		4.0		3.9		4.1
Moisture (%)		11.59		12.4		12.71
Volume Flow (acfm)		2,450,287		2,288,314		2,190,589
Temperature (°F)		1060		1102		1127
lb/hr		7.50		6.58		6.50
TPY		1.1		1.0		1.0
Lead (lb/hr)= Lead (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (2)		8.9		8.9		8.9
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		1.65E-02		1.46E-02		1.35E-02
TPY		2.47E-03		2.19E-03		2.03E-03

* corrected to 15% O2 dry conditions
+ corrected to dry conditions

Source: (1) General Electric, 1992; (2) EPA, 1990

Table A-3. Maximum Emissions of Other Regulated Pollutants for DESTEC Central Florida Cogeneration Facility
GE PG7221(FA), Dry Low NOx II Combustion System, Distillate Oil, Base Load

Pollutant	Units	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F
		Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F	
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Arsenic (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		4.2		4.2		4.2
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		7.77E-03		6.90E-03		6.37E-03
TPY		1.17E-03		1.04E-03		9.56E-04
Beryllium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		2.5		2.5		2.5
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		4.62E-03		4.11E-03		3.79E-03
TPY		6.94E-04		6.16E-04		5.69E-04
Mercury (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		3		3		3
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		5.55E-03		4.93E-03		4.55E-03
TPY		8.32E-04		7.39E-04		6.83E-04
Fluoride (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (2)		14		14		14
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		6.02E-02		5.35E-02		4.94E-02
TPY		9.03E-03		8.02E-03		7.41E-03
Sulfuric Acid Mist (lb/hr) = Fraction of SO2 Emission Rate x SO2 Emission Rate x lb H2SO4/lb SO2						
Fraction SO2 (%)		8		8		8
SO2 (lb/hr)		99.7		88.6		81.8
lb H2SO4/lb SO2 (98/64)		1.53		1.53		1.53
lb/hr		1.22E+01		1.08E+01		1.00E+01
TPY		1.83E+00		1.63E+00		1.50E+00

Note: Multiply by 2.324 to convert picogram/Joule (pg/J) to lb/10E+12 Btu.

Sources: (1) EPA, 1990; (2) EPA, 1980

Table A-4. Maximum Emissions of Non-Regulated Pollutants for DESTEC Central Florida Cogeneration Facility-
GE PG7221(FA), Dry Low NOx II Combustion System, Distillate Oil, Base Load

Pollutant	Units	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F
		Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F	
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Manganese (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		14		14		14
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		2.59E-02		2.30E-02		2.12E-02
TPY		3.88E-03		3.45E-03		3.19E-03
Nickel (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		170		170		170
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		3.14E-01		2.79E-01		2.58E-01
TPY		4.72E-02		4.19E-02		3.87E-02
Cadmium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		10.5		10.5		10.5
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		1.94E-02		1.73E-02		1.59E-02
TPY		2.91E-03		2.59E-03		2.39E-03
Chromium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		47.5		47.5		47.5
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		8.79E-02		7.80E-02		7.21E-02
TPY		1.32E-02		1.17E-02		1.08E-02
Copper (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		280		280		280
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		5.18E-01		4.60E-01		4.25E-01
TPY		7.77E-02		6.90E-02		6.37E-02
Vanadium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		69.5		69.5		69.5
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		1.29E-01		1.14E-01		1.05E-01
TPY		1.93E-02		1.71E-02		1.58E-02
Selenium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		23.42		23.42		23.42
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		4.33E-02		3.85E-02		3.55E-02
TPY		6.50E-03		5.77E-03		5.33E-03
Polycyclic Organic Matter (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		0.278		0.278		0.278
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		5.14E-04		4.57E-04		4.22E-04
TPY		7.71E-05		6.85E-05		6.33E-05
Formaldehyde (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		405		405		405
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		7.49E-01		6.65E-01		6.15E-01
TPY		1.12E-01		9.98E-02		9.22E-02

Source: (1) EPA, 1990

Table A-5. Maximum Emissions for Additional Non-Regulated Pollutant for DESTEC Central Florida Cogeneration Facility-
GE PG7221(FA), Dry Low NOx II Combustion System, Distillate Oil, Base Load

Pollutant	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F	
	Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F		
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Antimony (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		9.4		9.4		9.4
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		4.04E-02		3.59E-02		3.32E-02
TPY		6.06E-03		5.38E-03		4.97E-03
Barium (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		8.4		8.4		8.4
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		3.61E-02		3.21E-02		2.96E-02
TPY		5.42E-03		4.81E-03		4.44E-03
Cobalt (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		3.9		3.9		3.9
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		1.68E-02		1.49E-02		1.38E-02
TPY		2.51E-03		2.23E-03		2.06E-03
Zinc (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		294		294		294
HIR (MMBtu/hr)		1,849.9		1,642.9		1,517.6
lb/hr		1.26E+00		1.12E+00		1.04E+00
TPY		1.90E-01		1.68E-01		1.56E-01
Chlorine (lb/hr)= Basis (ppm) x Fuel oil (lb/hr) ÷ 1,000,000 (adj. for ppm)						
Basis, ppm		0.5		0.5		0.5
Fuel Oil (lb/hr)		99,722.9		88,568.4		81,812.7
lb/hr		4.99E-02		4.43E-02		4.09E-02
TPY		7.48E-03		6.64E-03		6.14E-03

Note: Multiply by 2.324 to convert picogram/Joule (pg/J) to lb/10E+12 Btu.

Source: (1) EPA, 1979

Table A-6. Design Information and Stack Parameters for DESTEC Central Florida Cogeneration Facility-
GE PG7221(FA), Dry Low NOx II Combustion System, Natural Gas, Base Load

Data	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F	
A	B	C	D	E	F	G
General						
Power (kW)	170,700.0	151,900.0	147,100.0	142,700.0	131,800.0	
Heat Rate (Btu/kwh)	9,460.0	9,750.0	9,860.0	9,970.0	10,230.0	
CT Exhaust Flow						
Mass Flow (lb/hr)	3,582,000	3,322,000	3,262,000	3,202,000	3,077,000	
Temperature (oF)	1,078	1,110	1,117	1,124	1,140	
Moisture (% Vol.)	7.61	8.83	9.21	10.05	9.91	
Oxygen (% Vol.)	12.71	12.56	12.51	12.36	12.48	
Molecular Weight	28.46	28.33	28.28	28.19	28.20	
Heat Input (MMBtu/hr)= Power (kW) x Heat Rate (Btu/kwh) ÷ 1,000,000 Btu/MMBtu						
Power (kW)	170,700.0	151,900.0	147,100.0	142,700.0	131,800.0	
Heat Rate (Btu/kwh)	9,460.0	9,750.0	9,860.0	9,970.0	10,230.0	
Heat Input (MMBtu/hr)	1,614.8	1,481.0	1,450.4	1,422.7	1,348.3	
Natural Gas Consumption (lb/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu ÷ Fuel Heat Content, LHV (Btu/lb)						
(cf/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu ÷ Fuel Heat Content, LHV (Btu/cf)						
Heat Input (MMBtu/hr)	1,614.8	1,481.0	1,450.4	1,422.7	1,348.3	
Heat Content, LHV (Btu/lb)	21,515	21,515	21,515	21,515	21,515	
Natural Gas (lb/hr)	75,055.6	68,836.9	67,413.7	66,126.8	62,668.6	
Heat Content, LHV (Btu/cf)	950	950	950	950	950	
Natural Gas (cf/hr)	1,699,813	1,558,974	1,526,743	1,497,599	1,419,278	
Volume Flow (acfm)= [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F)+ 460°F)] ÷ [Molecular weight x 2116.8] + 60 min/hr						
Mass Flow (lb/hr)	3,582,000	3,322,000	3,262,000	3,202,000	3,077,000	
Temperature (°F)	1,078	1,110	1,117	1,124	1,140	
Molecular Weight	28.46	28.33	28.28	28.19	28.20	
Volume Flow (acfm)	2,354,349	2,239,805	2,212,530	2,188,744	2,123,643	
Volume Flow (scfm)= [(Mass Flow (lb/hr) x 1,545 x (68°F + 460°F)] ÷ [Molecular weight x 2116.8] + 60 min/hr						
Mass Flow (lb/hr)	3,582,000	3,322,000	3,262,000	3,202,000	3,077,000	
Temperature (°F)	68	68	68	68	68	
Molecular Weight	28.46	28.33	28.28	28.19	28.20	
Volume Flow (scfm)	808,255	753,259	740,784	729,581	700,802	
HRSG Stack Data						
Stack Height (ft)	180	180	180	180	180	
Diameter (ft)	18.0	18.0	18.0	18.0	18.0	
Volume Flow (acfm) from HRSG= [Volume flow (acfm) x (HRSG temp.(°F)+ 460°F)] ÷ [CT temp.(°F)+ 460°F]						
Volume Flow (acfm) from CT	2,354,349	2,239,805	2,212,530	2,188,744	2,123,643	
CT Temperature (°F)	1,078	1,110	1,117	1,124	1,140	
HRSG Temperature (°F)	205	205	205	205	205	
Volume Flow (acfm) from HRSG	1,017,973	948,707	932,995	918,885	882,639	
Velocity (ft/sec)= Volume flow (acfm) from HRSG ÷ [(diameter)²+ 4) x 3.14159] + 60 sec/min						
Volume Flow (acfm) from HRSG	1,017,973	948,707	932,995	918,885	882,639	
Diameter (ft)	18.0	18.0	18.0	18.0	18.0	
Velocity (ft/sec)	66.7	62.1	61.1	60.2	57.8	

Note: Universal gas constant= 1,545 ft-lb(force)/°R; atmospheric pressure= 2,116.8 lb(force)/ft²

Source: General Electric, 1992.

Table A-7. Maximum Emissions for Criteria Pollutants for DESTEC Central Florida Cogeneration Facility-
GE PG7221(FA), Dry Low NOx II Combustion System, Natural Gas, Base Load

Pollutant	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F	
A	B	C	D	E	F	G
Hours of Operation		8460	8460	8460	8460	8460
Particulate (lb/hr)= Emission rate (lb/hr) from manufacturer						
Basis, lb/hr (manufactur.) (1)		9.0	9.0	9.0	9.0	9.0
lb/hr		9.0	9.0	9.0	9.0	9.0
TPY		38.07	38.07	38.07	38.07	38.07
Sulfur Dioxide (lb/hr)= Natural gas (cf/hr) x sulfur content(gr/100 cf) x 1 lb/7000 gr x (lb SO2/lb S) + 100						
Natural Gas (cf/hr)		1,699,813	1,558,974	1,526,743	1,497,599	1,419,278
Basis, gr/100 cf		1.0	1.0	1.0	1.0	1.0
lb SO2/lb S (64/32)		2.0	2.0	2.0	2.0	2.0
lb/hr		4.86	4.45	4.36	4.28	4.06
TPY		20.54	18.84	18.45	18.10	17.15
Nitrogen Oxides (lb/hr)= NOx(ppm) x [(20.9 x (1 - Moisture%)/100) - Oxygen(%)] x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr + [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		25.0	25.0	25.0	25.0	25.0
Moisture (%)		7.61	8.83	9.21	10.05	9.91
Oxygen (%)		12.71	12.56	12.51	12.36	12.48
Volume Flow (acfm)		2,354,349	2,239,805	2,212,530	2,188,744	2,123,643
Temperature (°F)		1078	1110	1117	1124	1140
lb/hr		161.9	148.5	145.3	142.6	135.0
TPY		684.72	627.98	614.78	603.09	571.14
Carbon Monoxide (lb/hr)= CO(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr + [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		15.0	15.0	15.0	15.0	15.0
Moisture (%)		7.61	8.83	9.21	10.05	9.91
Volume Flow (acfm)		2,354,349	2,239,805	2,212,530	2,188,744	2,123,643
Temperature (°F)		1078	1110	1117	1124	1140
lb/hr		48.8	44.9	44.0	42.9	41.3
TPY		206.55	189.96	186.03	181.52	174.63
VOCs (lb/hr)= VOC(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr + [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		1.5	1.5	1.5	1.6	1.5
Moisture (%)		7.61	8.83	9.21	10.05	9.91
Volume Flow (acfm)		2,354,349	2,239,805	2,212,530	2,188,744	2,123,643
Temperature (°F)		1078	1110	1117	1124	1140
lb/hr		2.79	2.57	2.51	2.62	2.36
TPY		11.80	10.85	10.63	11.06	9.98
Lead (lb/hr)= Negligible						
Basis, lb/10E+12 Btu		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA

* corrected to 15% O2 dry conditions
+ corrected to dry conditions

Source: General Electric, 1992.

Table A-8. Maximum Emissions of Other Regulated Pollutants for DESTEC Central Florida Cogeneration Facility
GE PG7221(FA), Dry Low NOx II Combustion System, Natural Gas, Base Load

Pollutant	Units	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F
A	B	C	D	E	F	G
Hours of Operation		8460	8460	8460	8460	8460
Arsenic (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Beryllium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Mercury (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Fluoride (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Sulfuric Acid Mist (lb/hr) = Fraction of SO2 Emission Rate x SO2 Emission Rate x lb H2SO4/lb SO2						
Fraction SO2 (%)		8	8	8	8	8
SO2 (lb/hr)		4.86	4.45	4.36	4.28	4.06
lb H2SO4/lb SO2 (98/64)		1.53	1.53	1.53	1.53	1.53
lb/hr		5.95E-01	5.46E-01	5.34E-01	5.24E-01	4.97E-01
TPY		2.52E+00	2.31E+00	2.26E+00	2.22E+00	2.10E+00

Source: (1) EPA, 1990

Table A-9. Maximum Emissions of Non-Regulated Pollutants for DESTEC Central Florida Cogeneration Facility-GE PG7221(FA), Dry Low NOx II Combustion System, Natural Gas, Base Load

Pollutant	Units	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F
A	B	C	D	E	F	G
Hours of Operation		8460	8460	8460	8460	8460
Manganese (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Nickel (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Cadmium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Chromium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Copper (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Vanadium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Selenium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Polycyclic Organic Matter (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		1.113	1.113	1.113	1.113	1.113
HIR (MMBtu/hr)		1,614.8	1,481.0	1,450.4	1,422.7	1,348.3
lb/hr		1.80E-03	1.65E-03	1.61E-03	1.58E-03	1.50E-03
TPY		7.60E-03	6.97E-03	6.83E-03	6.70E-03	6.35E-03
Formaldehyde (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		88.12	88.12	88.12	88.12	88.12
HIR (MMBtu/hr)		1,614.8	1,481.0	1,450.4	1,422.7	1,348.3
lb/hr		1.42E-01	1.31E-01	1.28E-01	1.25E-01	1.19E-01
TPY		6.02E-01	5.52E-01	5.41E-01	5.30E-01	5.03E-01

Source: (1) EPA, 1990

Table A-10. Maximum Emissions for Additional Non-Regulated Pollutant for DESTEC Central Florida Cogeneration Facility-
GE PG7221(FA), Dry Low NOx II Combustion System, Natural Gas, Base Load

Pollutant	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F	
A	B	C	D	E	F	G
Hours of Operation		8460		8460		8460
Antimony (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Barium (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Cobalt (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Zinc (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Chlorine (lb/hr)= Negligible						
Basis, ppm		NA	NA	NA	NA	NA
Natural gas (cf)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA

Table A-1A. Design Information and Stack Parameters for DESTEC Central Florida Cogeneration Facility-
GE PG7221(FA), Dry Low NOx II Combustion System, Distillate Oil, 70 Percent Load

Data	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F	
	Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F		
A	B	C	D	E	F	G
General						
Power (kW)		129,200.0		111,000.0		98,500.0
Heat Rate (Btu/kwh)		11,430.0		11,800.0		12,280.0
CT Exhaust Flow						
Mass Flow (lb/hr)		2,837,000		2,619,000		2,510,000
Temperature (oF)		1,166		1,192		1,200
Moisture (% Vol.)		11.96		12.40		12.48
Oxygen (% Vol.)		10.57		10.81		11.07
Molecular Weight		28.23		28.16		28.13
Heat Input (MMBtu/hr)= Power (kW) x Heat Rate (Btu/kwh) ÷ 1,000,000 Btu/MMBtu						
Power (kW)		129,200.0		111,000.0		98,500.0
Heat Rate (Btu/kwh)		11,430.0		11,800.0		12,280.0
Heat Input (MMBtu/hr)		1,476.8		1,309.8		1,209.6
Fuel Oil Consumption (lb/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu ÷ Fuel Heat Content, LHV (Btu/lb)						
Heat Input (MMBtu/hr)		1,476.8		1,309.8		1,209.6
Heat Content, LHV (Btu/lb)		18,550		18,550		18,550
Fuel Oil (lb/hr)		79,609.5		70,609.2		65,206.5
Volume Flow (acfm)= [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F)+ 460°F)] ÷ [Molecular weight x 2116.8] + 60 min/hr						
Mass Flow (lb/hr)		2,837,000		2,619,000		2,510,000
Temperature (°F)		1,166		1,192		1,200
Molecular Weight		28.23		28.16		28.13
Volume Flow (acfm)		1,988,010		1,869,045		1,802,083
Volume Flow (scfm)= [(Mass Flow (lb/hr) x 1,545 x (68°F + 460°F)] ÷ [Molecular weight x 2116.8] ÷ 60 min/hr						
Mass Flow (lb/hr)		2,837,000		2,619,000		2,510,000
Temperature (°F)		68		68		68
Molecular Weight		28.23		28.16		28.13
Volume Flow (scfm)		645,553		597,370		573,193
HRSG Stack Data						
Stack Height (ft)		180		180		180
Diameter (ft)		18.0		18.0		18.0
Volume Flow (acfm) from HRSG= [Volume flow (acfm) x (HRSG temp.(°F)+ 460°F)] ÷ [CT temp.(°F)+ 460°F]						
Volume Flow (acfm) from CT		1,988,010		1,869,045		1,802,083
CT Temperature (°F)		1,166		1,192		1,200
HRSG Temperature (°F)		200		200		200
Volume Flow (acfm) from HRSG		806,941		746,713		716,491
Velocity (ft/sec)= Volume flow (acfm) from HRSG ÷ [((diameter)²+ 4) x 3.14159] ÷ 60 sec/min						
Volume Flow (acfm) from HRSG		806,941		746,713		716,491
Diameter (ft)		18.0		18.0		18.0
Velocity (ft/sec)		52.9		48.9		46.9

Note: Universal gas constant= 1,545 ft-lb(force)/°R; atmospheric pressure= 2,116.8 lb(force)/ft²

Source: General Electric, 1992.

Table A-2A. Maximum Emissions for Criteria Pollutants for DESTEC Central Florida Cogeneration Facility-
GE PG7221(FA), Dry Low NOx II Combustion System, Distillate Oil, 70 Percent Load

Pollutant	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F	
	Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F		
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Particulate (lb/hr)= Emission rate (lb/hr) from manufacturer						
Basis, lb/hr (manufactur.) (1)		17.0		17.0		17.0
lb/hr		17.0		17.0		17.0
TPY		2.6		2.6		2.6
Sulfur Dioxide (lb/hr)= Fuel oil (lb/hr) x sulfur content(fraction) x (lb SO2/lb S) x fraction emitted as SO2						
Fuel Oil (lb/hr)		79,609.5		70,609.2		65,206.5
Sulfur content (%)		0.05		0.05		0.05
lb SO2/lb S (64/32)		2.0		2.0		2.0
SO2 Fraction emitted		1.00		1.00		1.00
lb/hr		79.61		70.61		65.21
TPY		11.9		10.6		9.8
Nitrogen Oxides (lb/hr)= NOx(ppm) x [(20.9 x (1 - Moisture%)/100) - Oxygen(%)] x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		42.0		42.0		42.0
Moisture (%)		11.96		12.4		12.48
Oxygen (%)		10.57		10.81		11.07
Volume Flow (acfm)		1,988,010		1,869,045		1,802,083
Temperature (°F)		1166		1192		1200
lb/hr		257.7		228.4		211.0
TPY		38.7		34.3		31.7
Carbon Monoxide (lb/hr)= CO(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		30.0		30.0		30.0
Moisture (%)		11.96		12.4		12.48
Volume Flow (acfm)		1,988,010		1,869,045		1,802,083
Temperature (°F)		1166		1192		1200
lb/hr		74.3		68.4		65.6
TPY		11.1		10.3		9.8
VOCs (lb/hr)= VOC(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		4.0		4.0		4.1
Moisture (%)		11.96		12.4		12.48
Volume Flow (acfm)		1,988,010		1,869,045		1,802,083
Temperature (°F)		1166		1192		1200
lb/hr		5.66		5.21		5.12
TPY		0.8		0.8		0.8
Lead (lb/hr)= Lead (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (2)		8.9		8.9		8.9
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		1.31E-02		1.17E-02		1.08E-02
TPY		1.97E-03		1.75E-03		1.61E-03

* corrected to 15% O2 dry conditions
+ corrected to dry conditions

Source: (1) General Electric, 1992; (2) EPA, 1990

Table A-3A. Maximum Emissions of Other Regulated Pollutants for DESTEC Central Florida Cogeneration Facility
GE PG7221(FA), Dry Low NOx II Combustion System, Distillate Oil, 70 Percent Load

Pollutant	Units	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F
		Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F	
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Arsenic (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		4.2		4.2		4.2
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		6.20E-03		5.50E-03		5.08E-03
TPY		9.30E-04		8.25E-04		7.62E-04
Beryllium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		2.5		2.5		2.5
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		3.69E-03		3.27E-03		3.02E-03
TPY		5.54E-04		4.91E-04		4.54E-04
Mercury (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		3		3		3
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		4.43E-03		3.93E-03		3.63E-03
TPY		6.65E-04		5.89E-04		5.44E-04
Fluoride (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (2)		14		14		14
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		4.80E-02		4.26E-02		3.94E-02
TPY		7.21E-03		6.39E-03		5.90E-03
Sulfuric Acid Mist (lb/hr) = Fraction of SO2 Emission Rate x SO2 Emission Rate x lb H2SO4/lb SO2						
Fraction SO2 (%)		8		8		8
SO2 (lb/hr)		79.6		70.6		65.2
lb H2SO4/lb SO2 (98/64)		1.53		1.53		1.53
lb/hr		9.75E+00		8.65E+00		7.99E+00
TPY		1.46E+00		1.30E+00		1.20E+00

Note: Multiply by 2.324 to convert picogram/Joule (pg/J) to lb/10E+12 Btu.

Sources: (1) EPA, 1990; (2) EPA, 1980

Table A-4A. Maximum Emissions of Non-Regulated Pollutants for DESTEC Central Florida Cogeneration Facility-
GE PG7221(FA), Dry Low NOx II Combustion System, Distillate Oil, 70 Percent Load

Pollutant	Units	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F
		Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F	
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Manganese (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		14		14		14
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		2.07E-02		1.83E-02		1.69E-02
TPY		3.10E-03		2.75E-03		2.54E-03
Nickel (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		170		170		170
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		2.51E-01		2.23E-01		2.06E-01
TPY		3.77E-02		3.34E-02		3.08E-02
Cadmium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		10.5		10.5		10.5
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		1.55E-02		1.38E-02		1.27E-02
TPY		2.33E-03		2.06E-03		1.91E-03
Chromium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		47.5		47.5		47.5
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		7.01E-02		6.22E-02		5.75E-02
TPY		1.05E-02		9.33E-03		8.62E-03
Copper (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		280		280		280
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		4.13E-01		3.67E-01		3.39E-01
TPY		6.20E-02		5.50E-02		5.08E-02
Vanadium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		69.5		69.5		69.5
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		1.03E-01		9.10E-02		8.41E-02
TPY		1.54E-02		1.37E-02		1.26E-02
Selenium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		23.42		23.42		23.42
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		3.46E-02		3.07E-02		2.83E-02
TPY		5.19E-03		4.60E-03		4.25E-03
Polycyclic Organic Matter (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		0.278		0.278		0.278
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		4.11E-04		3.64E-04		3.36E-04
TPY		6.16E-05		5.46E-05		5.04E-05
Formaldehyde (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		405		405		405
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		5.98E-01		5.30E-01		4.90E-01
TPY		8.97E-02		7.96E-02		7.35E-02

Source: (1) EPA, 1990

Table A-5A. Maximum Emissions for Additional Non-Regulated Pollutant for DESTEC Central Florida Cogeneration Facility-GE PG7221(FA), Dry Low NOx II Combustion System, Distillate Oil, 70 Percent Load

Pollutant	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F	
	Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F		
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Antimony (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		9.4		9.4		9.4
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		3.23E-02		2.86E-02		2.64E-02
TPY		4.84E-03		4.29E-03		3.96E-03
Barium (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		8.4		8.4		8.4
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		2.88E-02		2.56E-02		2.36E-02
TPY		4.32E-03		3.84E-03		3.54E-03
Cobalt (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		3.9		3.9		3.9
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		1.34E-02		1.19E-02		1.10E-02
TPY		2.01E-03		1.78E-03		1.64E-03
Zinc (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		294		294		294
HIR (MMBtu/hr)		1,476.8		1,309.8		1,209.6
lb/hr		1.01E+00		8.95E-01		8.26E-01
TPY		1.51E-01		1.34E-01		1.24E-01
Chlorine (lb/hr)= Basis (ppm) x Fuel oil (lb/hr) ÷ 1,000,000 (adj. for ppm)						
Basis, ppm		0.5		0.5		0.5
Fuel Oil (lb/hr)		79,609.5		70,609.2		65,206.5
lb/hr		3.98E-02		3.53E-02		3.26E-02
TPY		5.97E-03		5.30E-03		4.89E-03

Note: Multiply by 2.324 to convert picogram/Joule (pg/J) to lb/10E+12 Btu.

Source: (1) EPA, 1979

Table A-6A. Design Information and Stack Parameters for DESTEC Central Florida Cogeneration Facility-
GE PG7221(FA), Dry Low NOx II Combustion System, Natural Gas, 70 Percent Load

Data	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F	
A	B	C	D	E	F	G
General						
Power (kW)		119,900.0	106,500.0	103,100.0	99,500.0	90,900.0
Heat Rate (Btu/kwh)		10,770.0	11,070.0	11,340.0	11,510.0	11,890.0
CT Exhaust Flow						
Mass Flow (lb/hr)		2,744,000	2,595,000	2,560,000	2,524,000	2,454,000
Temperature (oF)		1,177	1,195	1,199	1,200	1,200
Moisture (% Vol.)		7.84	8.98	9.34	10.14	9.89
Oxygen (% Vol.)		12.46	12.41	12.39	12.28	12.52
Molecular Weight		28.45	28.32	28.27	28.18	28.20
Heat Input (MMBtu/hr)= Power (kW) x Heat Rate (Btu/kwh) + 1,000,000 Btu/MMBtu						
Power (kW)		119,900.0	106,500.0	103,100.0	99,500.0	90,900.0
Heat Rate (Btu/kwh)		10,770.0	11,070.0	11,340.0	11,510.0	11,890.0
Heat Input (MMBtu/hr)		1,291.3	1,179.0	1,169.2	1,145.2	1,080.8
Natural Gas Consumption (lb/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu + Fuel Heat Content, LHV (Btu/lb) (cf/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu + Fuel Heat Content, LHV (Btu/cf)						
Heat Input (MMBtu/hr)		1,291.3	1,179.0	1,169.2	1,145.2	1,080.8
Heat Content, LHV (Btu/lb)		21,515	21,515	21,515	21,515	21,515
Natural Gas (lb/hr)		60,019.7	54,796.9	54,341.3	53,230.1	50,234.8
Heat Content, LHV (Btu/cf)		950	950	950	950	950
Natural Gas (cf/hr)		1,359,287	1,241,005	1,230,688	1,205,521	1,137,685
Volume Flow (acfm)= [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F)+ 460°F)] ÷ [Molecular weight x 2116.8] ÷ 60 min/hr						
Mass Flow (lb/hr)		2,744,000	2,595,000	2,560,000	2,524,000	2,454,000
Temperature (°F)		1,177	1,195	1,199	1,200	1,200
Molecular Weight		28.45	28.32	28.27	28.18	28.20
Volume Flow (acfm)		1,920,685	1,845,077	1,827,352	1,808,470	1,757,157
Volume Flow (scfm)= [(Mass Flow (lb/hr) x 1,545 x (68°F + 460°F)] ÷ [Molecular weight x 2116.8] ÷ 60 min/hr						
Mass Flow (lb/hr)		2,744,000	2,595,000	2,560,000	2,524,000	2,454,000
Temperature (°F)		68	68	68	68	68
Molecular Weight		28.45	28.32	28.27	28.18	28.20
Volume Flow (scfm)		619,500	588,641	581,580	575,224	558,903
HRSG Stack Data						
Stack Height (ft)		180	180	180	180	180
Diameter (ft)		18.0	18.0	18.0	18.0	18.0
Volume Flow (acfm) from HRSG= [Volume flow (acfm) x (HRSG temp.(°F)+ 460°F)] ÷ [CT temp.(°F)+ 460°F]						
Volume Flow (acfm) from CT		1,920,685	1,845,077	1,827,352	1,808,470	1,757,157
CT Temperature (°F)		1,177	1,195	1,199	1,200	1,200
HRSG Temperature (°F)		200	200	200	200	200
Volume Flow (acfm) from HRSG		774,375	735,801	726,975	719,030	698,629
Velocity (ft/sec)= Volume flow (acfm) from HRSG ÷ [((diameter)² + 4) x 3.14159] ÷ 60 sec/min						
Volume Flow (acfm) from HRSG		774,375	735,801	726,975	719,030	698,629
Diameter (ft)		18.0	18.0	18.0	18.0	18.0
Velocity (ft/sec)		50.7	48.2	47.6	47.1	45.8

Note: Universal gas constant= 1,545 ft-lb(force)/°R; atmospheric pressure= 2,116.8 lb(force)/ft²

Source: General Electric, 1992.

Table A-7A. Maximum Emissions for Criteria Pollutants for DESTEC Central Florida Cogeneration Facility-
GE PG7221(FA), Dry Low NOx II Combustion System, Natural Gas, 70 Percent Load

Pollutant	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F	
A	B	C	D	E	F	G
Hours of Operation		8460	8460	8460	8460	8460
Particulate (lb/hr)= Emission rate (lb/hr) from manufacturer						
Basis, lb/hr (manufactur.) (1)		9.0	9.0	9.0	9.0	9.0
lb/hr		9.0	9.0	9.0	9.0	9.0
TPY		38.07	38.07	38.07	38.07	38.07
Sulfur Dioxide (lb/hr)= Natural gas (cf/hr) x sulfur content(gr/100 cf) x 1 lb/7000 gr x (lb SO2/lb S) + 100						
Natural Gas (cf/hr)		1,359,287	1,241,005	1,230,688	1,205,521	1,137,685
Basis, gr/100 cf		1.0	1.0	1.0	1.0	1.0
lb SO2/lb S (64/32)		2.0	2.0	2.0	2.0	2.0
lb/hr		3.88	3.55	3.52	3.44	3.25
TPY		16.43	15.00	14.87	14.57	13.75
Nitrogen Oxides (lb/hr)= NOx(ppm) x [(20.9 x (1 - Moisture%/100)) - Oxygen(%) x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		25.0	25.0	25.0	25.0	25.0
Moisture (%)		7.84	8.98	9.34	10.14	9.89
Oxygen (%)		12.46	12.41	12.39	12.28	12.52
Volume Flow (acfm)		1,920,685	1,845,077	1,827,352	1,808,470	1,757,157
Temperature (°F)		1177	1195	1199	1200	1200
lb/hr		127.9	118.1	115.7	113.5	107.1
TPY		540.88	499.71	489.59	480.01	452.93
Carbon Monoxide (lb/hr)= CO(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm+ (1)		15.0	15.0	15.0	15.0	15.0
Moisture (%)		7.84	8.98	9.34	10.14	9.89
Volume Flow (acfm)		1,920,685	1,845,077	1,827,352	1,808,470	1,757,157
Temperature (°F)		1177	1195	1199	1200	1200
lb/hr		37.3	35.0	34.5	33.8	32.9
TPY		157.92	148.20	145.84	142.98	139.31
VOCs (lb/hr)= VOC(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm+ (1)		1.5	1.5	1.5	1.6	1.5
Moisture (%)		7.84	8.98	9.34	10.14	9.89
Volume Flow (acfm)		1,920,685	1,845,077	1,827,352	1,808,470	1,757,157
Temperature (°F)		1177	1195	1199	1200	1200
lb/hr		2.13	2.00	2.00	2.06	1.88
TPY		9.02	8.47	8.44	8.71	7.96
Lead (lb/hr)= Negligible						
Basis, lb/10E+12 Btu		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA

* corrected to 15% O2 dry conditions
+ corrected to dry conditions

Source: General Electric, 1992.

Table A-8A. Maximum Emissions of Other Regulated Pollutants for DESTEC Central Florida Cogeneration Facility
GE PG7221(FA), Dry Low NOx II Combustion System, Natural Gas, 70 Percent Load

Pollutant	Units	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F
A	B	C	D	E	F	G
Hours of Operation		8460	8460	8460	8460	8460
Arsenic (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Beryllium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Mercury (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Fluoride (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Sulfuric Acid Mist (lb/hr) = Fraction of SO2 Emission Rate x SO2 Emission Rate x lb H2SO4/lb SO2						
Fraction SO2 (%)		8	8	8	8	8
SO2 (lb/hr)		3.88	3.55	3.52	3.44	3.25
lb H2SO4/lb SO2 (98/64)		1.53	1.53	1.53	1.53	1.53
lb/hr		4.76E-01	4.34E-01	4.31E-01	4.22E-01	3.98E-01
TPY		2.01E+00	1.84E+00	1.82E+00	1.78E+00	1.68E+00

Source: (1) EPA, 1990

Table A-9A. Maximum Emissions of Non-Regulated Pollutants for DESTEC Central Florida Cogeneration Facility-GE PG7221(FA), Dry Low NOx II Combustion System, Natural Gas, 70 Percent Load

Pollutant	Units	Gas Turbine	Gas Turbine	Gas Turbine	Gas Turbine	Gas Turbine
		Natural Gas 27 °F	Natural Gas 64 °F	Natural Gas 72 °F	Natural Gas 79 °F	Natural Gas 97 °F
A	B	C	D	E	F	G
Hours of Operation		8460	8460	8460	8460	8460
Manganese (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Nickel (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Cadmium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Chromium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Copper (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Vanadium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Selenium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Polycyclic Organic Matter (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		1.113	1.113	1.113	1.113	1.113
HIR (MMBtu/hr)		1,291.3	1,179.0	1,169.2	1,145.2	1,080.8
lb/hr		1.44E-03	1.31E-03	1.30E-03	1.27E-03	1.20E-03
TPY		6.08E-03	5.55E-03	5.50E-03	5.39E-03	5.09E-03
Formaldehyde (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		88.12	88.12	88.12	88.12	88.12
HIR (MMBtu/hr)		1,291.3	1,179.0	1,169.2	1,145.2	1,080.8
lb/hr		1.14E-01	1.04E-01	1.03E-01	1.01E-01	9.52E-02
TPY		4.81E-01	4.39E-01	4.36E-01	4.27E-01	4.03E-01

Source: (1) EPA, 1990

Table A-10A. Maximum Emissions for Additional Non-Regulated Pollutant for DESTEC Central Florida Cogeneration Facility-
GE PG7221(FA), Dry Low NOx II Combustion System, Natural Gas, 70 Percent Load

Pollutant		Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F
A	B	C	D	E	F	G
Hours of Operation		8460		8460		8460
Antimony (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Barium (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Cobalt (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Zinc (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Chlorine (lb/hr)= Negligible						
Basis, ppm		NA	NA	NA	NA	NA
Natural gas (cf)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA

Table A-19. Design Information and Stack Parameters for DESTEC Central Florida Cogeneration Facility-
Westinghouse 501F, Conventional Combustor, Distillate Oil, Base Load

Data	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F	
	Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F		
A	B	C	D	E	F	G
General						
Power (kW)		171,970.0		162,330.0		147,180.0
Heat Rate (Btu/kwh)		9,280.0		9,560.0		9,850.0
CT Exhaust Flow						
Mass Flow (lb/hr)		3,502,180		3,509,380		3,311,800
Temperature (oF)		1,104		1,104		1,121
Moisture (% Vol.)		10.60		11.91		12.57
Oxygen (% Vol.)		11.92		11.88		11.83
Molecular Weight		28.33		28.17		28.09
Heat Input (MMBtu/hr)= Power (kW) x Heat Rate (Btu/kwh) ÷ 1,000,000 Btu/MMBtu						
Power (kW)		171,970.0		162,330.0		147,180.0
Heat Rate (Btu/kwh)		9,280.0		9,560.0		9,850.0
Heat Input (MMBtu/hr)		1,595.9		1,551.9		1,449.7
Fuel Oil Consumption (lb/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu ÷ Fuel Heat Content, LHV (Btu/lb)						
Heat Input (MMBtu/hr)		1,595.9		1,551.9		1,449.7
Heat Content, LHV (Btu/lb)		18,450		18,450		18,450
Fuel Oil (lb/hr)		86,497.6		84,112.5		78,575.8
Volume Flow (acfm)= [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F)+ 460°F)] ÷ [Molecular weight x 2116.8] ÷ 60 min/hr						
Mass Flow (lb/hr)		3,502,180		3,509,380		3,311,800
Temperature (°F)		1,104		1,104		1,121
Molecular Weight		28.33		28.17		28.09
Volume Flow (acfm)		2,351,909		2,370,209		2,267,804
Volume Flow (scfm)= [(Mass Flow (lb/hr) x 1,545 x (68°F + 460°F)] ÷ [Molecular weight x 2116.8] ÷ 60 min/hr						
Mass Flow (lb/hr)		3,502,180		3,509,380		3,311,800
Temperature (°F)		68		68		68
Molecular Weight		28.33		28.17		28.09
Volume Flow (scfm)		793,995		800,173		757,369
HRSG Stack Data						
Stack Height (ft)		180		180		180
Diameter (ft)		18.0		18.0		18.0
Volume Flow (acfm) from HRSG= [Volume flow (acfm) x (HRSG temp.(°F)+ 460°F)] ÷ [CT temp.(°F)+ 460°F]						
Volume Flow (acfm) from CT		2,351,909		2,370,209		2,267,804
CT Temperature (°F)		1,104		1,104		1,121
HRSG Temperature (°F)		205		205		205
Volume Flow (acfm) from HRSG		1,000,012		1,007,794		953,883
Velocity (ft/sec)= Volume flow (acfm) from HRSG ÷ [((diameter)² ÷ 4) x 3.14159] ÷ 60 sec/min						
Volume Flow (acfm) from HRSG		1,000,012		1,007,794		953,883
Diameter (ft)		18.0		18.0		18.0
Velocity (ft/sec)		65.5		66.0		62.5

Note: Universal gas constant= 1,545 ft-lb(force)/°R; atmospheric pressure= 2,116.8 lb(force)/ft²

Source: Westinghouse, 1992.

Table A-20. Maximum Emissions for Criteria Pollutants for DESTEC Central Florida Cogeneration Facility-
Westinghouse 501F, Conventional Combustor, Distillate Oil, Base Load

Pollutant	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F	
	Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F		
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Particulate (lb/hr)= Emission rate (lb/hr) from manufacturer						
Basis, lb/hr (manufactur.) (1)		39.5		39.0		36.7
lb/hr		39.5		39.0		36.7
TPY		5.9		5.9		5.5
Sulfur Dioxide (lb/hr)= Fuel oil (lb/hr) x sulfur content(fraction) x (lb SO2/lb S) x fraction emitted as SO2						
Fuel Oil (lb/hr)		86,497.6		84,112.5		78,575.8
Sulfur content (%)		0.05		0.05		0.05
lb SO2/lb S (64/32)		2.0		2.0		2.0
SO2 Fraction emitted		1.00		1.00		1.00
lb/hr		89.35		86.22		81.33
TPY		13.4		12.9		12.2
Nitrogen Oxides (lb/hr)= NOx(ppm) x [(20.9 x (1 - Moisture%/100)) - Oxygen(%)] x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		44.5		42.7		42.7
Moisture (%)		10.6		11.91		12.57
Oxygen (%)		11.92		11.88		11.83
Volume Flow (acfm)		2,351,909		2,370,209		2,267,804
Temperature (°F)		1104		1104		1121
lb/hr		290.1		270.9		252.9
TPY		43.5		40.6		37.9
Carbon Monoxide (lb/hr)= CO(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		52.0		51.6		51.5
Moisture (%)		10.6		11.91		12.57
Volume Flow (acfm)		2,351,909		2,370,209		2,267,804
Temperature (°F)		1104		1104		1121
lb/hr		160.9		158.4		148.7
TPY		24.1		23.8		22.3
VOCs (lb/hr)= VOC(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		10.6		10.5		10.5
Moisture (%)		10.6		11.91		12.57
Volume Flow (acfm)		2,351,909		2,370,209		2,267,804
Temperature (°F)		1104		1104		1121
lb/hr		18.74		18.44		17.32
TPY		2.8		2.8		2.6
Lead (lb/hr)= Lead (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (2)		8.9		8.9		8.9
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		1.42E-02		1.38E-02		1.29E-02
TPY		2.13E-03		2.07E-03		1.94E-03

* corrected to 15% O2 dry conditions
+ corrected to dry conditions

Source: (1) Westinghouse, 1992; (2) EPA, 1990

Table A-21. Maximum Emissions of Other Regulated Pollutants for DESTEC Central Florida Cogeneration Facility Westinghouse 501F, Conventional Combustor, Distillate Oil, Base Load

Pollutant	Units	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F
		Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F	
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Arsenic (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		4.2		4.2		4.2
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		6.70E-03		6.52E-03		6.09E-03
TPY		1.01E-03		9.78E-04		9.13E-04
Beryllium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		2.5		2.5		2.5
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		3.99E-03		3.88E-03		3.62E-03
TPY		5.98E-04		5.82E-04		5.44E-04
Mercury (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		3		3		3
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		4.79E-03		4.66E-03		4.35E-03
TPY		7.18E-04		6.98E-04		6.52E-04
Fluoride (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (2)		14		14		14
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		5.19E-02		5.05E-02		4.72E-02
TPY		7.79E-03		7.57E-03		7.08E-03
Sulfuric Acid Mist (lb/hr) = Fraction of SO2 Emission Rate x SO2 Emission Rate x lb H2SO4/lb SO2						
Fraction SO2 (%)		8		8		8
SO2 (lb/hr)		89.4		86.2		81.3
lb H2SO4/lb SO2 (98/64)		1.53		1.53		1.53
lb/hr		1.09E+01		1.06E+01		9.96E+00
TPY		1.64E+00		1.58E+00		1.49E+00

Note: Multiply by 2.324 to convert picogram/Joule (pg/J) to lb/10E+12 Btu.

Sources: (1) EPA, 1990; (2) EPA, 1980

Table A-22. Maximum Emissions of Non-Regulated Pollutants for DESTEC Central Florida Cogeneration Facility-
Westinghouse 501F, Conventional Combustor, Distillate Oil, Base Load

Pollutant	Units	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F
		Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F	
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Manganese (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		14		14		14
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		2.23E-02		2.17E-02		2.03E-02
TPY		3.35E-03		3.26E-03		3.04E-03
Nickel (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		170		170		170
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		2.71E-01		2.64E-01		2.46E-01
TPY		4.07E-02		3.96E-02		3.70E-02
Cadmium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		10.5		10.5		10.5
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		1.68E-02		1.63E-02		1.52E-02
TPY		2.51E-03		2.44E-03		2.28E-03
Chromium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		47.5		47.5		47.5
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		7.58E-02		7.37E-02		6.89E-02
TPY		1.14E-02		1.11E-02		1.03E-02
Copper (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		280		280		280
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		4.47E-01		4.35E-01		4.06E-01
TPY		6.70E-02		6.52E-02		6.09E-02
Vanadium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		69.5		69.5		69.5
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		1.11E-01		1.08E-01		1.01E-01
TPY		1.66E-02		1.62E-02		1.51E-02
Selenium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		23.42		23.42		23.42
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		3.74E-02		3.63E-02		3.40E-02
TPY		5.61E-03		5.45E-03		5.09E-03
Polycyclic Organic Matter (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		0.278		0.278		0.278
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		4.44E-04		4.31E-04		4.03E-04
TPY		6.65E-05		6.47E-05		6.05E-05
Formaldehyde (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		405		405		405
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		6.46E-01		6.29E-01		5.87E-01
TPY		9.69E-02		9.43E-02		8.81E-02

Source: (1) EPA, 1990

Table A-23. Maximum Emissions for Additional Non-Regulated Pollutant for DESTEC Central Florida Cogeneration Facility- Westinghouse 501F, Conventional Combustor, Distillate Oil, Base Load

Pollutant	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F	
	Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F		
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Antimony (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		9.4		9.4		9.4
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		3.49E-02		3.39E-02		3.17E-02
TPY		5.23E-03		5.09E-03		4.75E-03
Barium (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		8.4		8.4		8.4
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		3.12E-02		3.03E-02		2.83E-02
TPY		4.67E-03		4.54E-03		4.25E-03
Cobalt (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		3.9		3.9		3.9
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		1.45E-02		1.41E-02		1.31E-02
TPY		2.17E-03		2.11E-03		1.97E-03
Zinc (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		294		294		294
HIR (MMBtu/hr)		1,595.9		1,551.9		1,449.7
lb/hr		1.09E+00		1.06E+00		9.91E-01
TPY		1.64E-01		1.59E-01		1.49E-01
Chlorine (lb/hr)= Basis (ppm) x Fuel oil (lb/hr) ÷ 1,000,000 (adj. for ppm)						
Basis, ppm		0.5		0.5		0.5
Fuel Oil (lb/hr)		86,497.6		84,112.5		78,575.8
lb/hr		4.32E-02		4.21E-02		3.93E-02
TPY		6.49E-03		6.31E-03		5.89E-03

Note: Multiply by 2.324 to convert picogram/Joule (pg/J) to lb/10E+12 Btu.

Table A-24. Design Information and Stack Parameters for DESTEC Central Florida Cogeneration Facility-
Westinghouse 501F, Dry Low NOx Combustor, Natural Gas, Base Load

Data	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F	
A	B	C	D	E	F	G
General						
Power (kW)		169,210.0	147,950.0	143,450.0	139,500.0	129,370.0
Heat Rate (Btu/kwh)		9,490.0	9,900.0	10,000.0	10,100.0	10,360.0
CT Exhaust Flow						
Mass Flow (lb/hr)		3,702,540	3,431,310	3,369,010	3,311,770	3,180,510
Temperature (oF)		1,063	1,086	1,092	1,098	1,111
Moisture (% Vol.)		7.26	8.45	8.82	9.32	9.56
Oxygen (% Vol.)		13.08	12.97	12.91	12.82	12.84
Molecular Weight		28.49	28.36	28.32	28.26	28.23
Heat Input (MMBtu/hr)= Power (kW) x Heat Rate (Btu/kwh) ÷ 1,000,000 Btu/MMBtu						
Power (kW)		169,210.0	147,950.0	143,450.0	139,500.0	129,370.0
Heat Rate (Btu/kwh)		9,490.0	9,900.0	10,000.0	10,100.0	10,360.0
Heat Input (MMBtu/hr)		1,605.8	1,464.7	1,434.5	1,409.0	1,340.3
Natural Gas Consumption (lb/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu ÷ Fuel Heat Content, LHV (Btu/lb) (cf/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu ÷ Fuel Heat Content, LHV (Btu/cf)						
Heat Input (MMBtu/hr)		1,605.8	1,464.7	1,434.5	1,409.0	1,340.3
Heat Content, LHV (Btu/lb)		20,900	20,900	20,900	20,900	20,900
Natural Gas (lb/hr)		76,832.7	70,081.6	68,636.4	67,413.9	64,127.9
Heat Content, LHV (Btu/cf)		950	950	950	950	950
Natural Gas (cf/hr)		1,690,319	1,541,795	1,510,000	1,483,105	1,410,814
Volume Flow (acfm)= [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F)+ 460°F)] ÷ [Molecular weight x 2116.8] + 60 min/hr						
Mass Flow (lb/hr)		3,702,540	3,431,310	3,369,010	3,311,770	3,180,510
Temperature (°F)		1,063	1,086	1,092	1,098	1,111
Molecular Weight		28.49	28.36	28.32	28.26	28.23
Volume Flow (acfm)		2,407,465	2,275,544	2,246,146	2,221,160	2,152,966
Volume Flow (scfm)= [(Mass Flow (lb/hr) x 1,545 x (68°F + 460°F)] ÷ [Molecular weight x 2116.8] + 60 min/hr						
Mass Flow (lb/hr)		3,702,540	3,431,310	3,369,010	3,311,770	3,180,510
Temperature (°F)		68	68	68	68	68
Molecular Weight		28.49	28.36	28.32	28.26	28.23
Volume Flow (scfm)		834,630	777,159	764,153	752,742	723,594
HRSG Stack Data						
Stack Height (ft)		180	180	180	180	180
Diameter (ft)		18.0	18.0	18.0	18.0	18.0
Volume Flow (acfm) from HRSG= [Volume flow (acfm) x (HRSG temp.(°F)+ 460°F)] ÷ [CT temp.(°F)+ 460°F]						
Volume Flow (acfm) from CT		2,407,465	2,275,544	2,246,146	2,221,160	2,152,966
CT Temperature (°F)		1,063	1,086	1,092	1,098	1,111
HRSG Temperature (°F)		205	205	205	205	205
Volume Flow (acfm) from HRSG		1,051,191	978,808	962,427	948,056	911,345
Velocity (ft/sec)= Volume flow (acfm) from HRSG ÷ [((diameter)² ÷ 4) x 3.14159] ÷ 60 sec/min						
Volume Flow (acfm) from HRSG		1,051,191	978,808	962,427	948,056	911,345
Diameter (ft)		18.0	18.0	18.0	18.0	18.0
Velocity (ft/sec)		68.8	64.1	63.0	62.1	59.7

Note: Universal gas constant= 1,545 ft-lb(force)/°R; atmospheric pressure= 2,116.8 lb(force)/ft²

Source: Westinghouse, 1992.

Table A-25. Maximum Emissions for Criteria Pollutants for DESTEC Central Florida Cogeneration Facility- Westinghouse 501F, Dry Low NOx Combustor, Natural Gas, Base Load

Pollutant	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F	
A	B	C	D	E	F	G
Hours of Operation		8460	8460	8460	8460	8460
Particulate (lb/hr)= Emission rate (lb/hr) from manufacturer						
Basis, lb/hr (manufactur.) (1)		6.60	6.10	6.00	5.90	5.70
lb/hr		6.60	6.10	6.00	5.90	5.70
TPY		27.92	25.80	25.38	24.96	24.11
Sulfur Dioxide (lb/hr)= Natural gas (cf/hr) x sulfur content(gr/100 cf) x 1 lb/7000 gr x (lb SO2/lb S) ÷ 100						
Natural Gas (cf/hr)		1,690,319	1,541,795	1,510,000	1,483,105	1,410,814
Basis, gr/100 cf		1.0	1.0	1.0	1.0	1.0
lb SO2/lb S (64/32)		2.0	2.0	2.0	2.0	2.0
lb/hr		4.83	4.41	4.31	4.24	4.03
TPY		20.43	18.63	18.25	17.92	17.05
Nitrogen Oxides (lb/hr)= NOx(ppm) x [(20.9 x (1 - Moisture%/100)) - Oxygen(%)] x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		25.5	25.5	25.4	25.5	25.5
Moisture (%)		7.26	8.45	8.82	9.32	9.56
Oxygen (%)		13.08	12.97	12.91	12.82	12.84
Volume Flow (acfm)		2,407,465	2,275,544	2,246,146	2,221,160	2,152,966
Temperature (°F)		1063	1086	1092	1098	1111
lb/hr		162.8	148.3	144.8	142.9	135.8
TPY		688.77	627.23	612.58	604.38	574.33
Carbon Monoxide (lb/hr)= CO(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		10.3	10.4	10.3	10.4	10.2
Moisture (%)		7.26	8.45	8.82	9.32	9.56
Volume Flow (acfm)		2,407,465	2,275,544	2,246,146	2,221,160	2,152,966
Temperature (°F)		1063	1086	1092	1098	1111
lb/hr		34.8	32.3	31.3	30.9	29.1
TPY		147.02	136.45	132.34	130.91	123.09
VOCs (lb/hr)= VOC(ppm) x [1 - Moisture%/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		4.2	4.0	4.1	4.1	4.3
Moisture (%)		7.26	8.45	8.82	9.32	9.56
Volume Flow (acfm)		2,407,465	2,275,544	2,246,146	2,221,160	2,152,966
Temperature (°F)		1063	1086	1092	1098	1111
lb/hr		8.10	7.09	7.12	6.97	7.01
TPY		34.26	29.99	30.10	29.49	29.65
Lead (lb/hr)= Negligible						
Basis, lb/10E+12 Btu		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA

* corrected to 15% O2 dry conditions
+ corrected to dry conditions

Table A-26. Maximum Emissions of Other Regulated Pollutants for DESTEC Central Florida Cogeneration Facility Westinghouse 501F, Dry Low NOx Combustor, Natural Gas, Base Load

Pollutant	Units	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F
A	B	C	D	E	F	G
Hours of Operation		8460	8460	8460	8460	8460
Arsenic (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Beryllium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Mercury (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Fluoride (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Sulfuric Acid Mist (lb/hr) = Fraction of SO2 Emission Rate x SO2 Emission Rate x lb H2SO4/lb SO2						
Fraction SO2 (%)		8	8	8	8	8
SO2 (lb/hr)		4.83	4.41	4.31	4.24	4.03
lb H2SO4/lb SO2 (98/64)		1.53	1.53	1.53	1.53	1.53
lb/hr		6.23E-01	5.68E-01	5.56E-01	5.46E-01	5.20E-01
TPY		2.63E+00	2.40E+00	2.35E+00	2.31E+00	2.20E+00

Source: (1) EPA, 1990

Table A-27. Maximum Emissions of Non-Regulated Pollutants for DESTEC Central Florida Cogeneration Facility-
Westinghouse 501F, Dry Low NOx Combustor, Natural Gas, Base Load

Pollutant	Units	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F
A	B	C	D	E	F	G
Hours of Operation		8460	8460	8460	8460	8460
Manganese (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Nickel (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Cadmium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Chromium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Copper (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Vanadium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Selenium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Polycyclic Organic Matter (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		1.113	1.113	1.113	1.113	1.113
HIR (MMBtu/hr)		1,605.8	1,464.7	1,434.5	1,409.0	1,340.3
lb/hr		1.79E-03	1.63E-03	1.60E-03	1.57E-03	1.49E-03
TPY		7.56E-03	6.90E-03	6.75E-03	6.63E-03	6.31E-03
Formaldehyde (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		88.12	88.12	88.12	88.12	88.12
HIR (MMBtu/hr)		1,605.8	1,464.7	1,434.5	1,409.0	1,340.3
lb/hr		1.42E-01	1.29E-01	1.26E-01	1.24E-01	1.18E-01
TPY		5.99E-01	5.46E-01	5.35E-01	5.25E-01	5.00E-01

Source: (1) EPA, 1990

Table A-28. Maximum Emissions for Additional Non-Regulated Pollutant for DESTEC Central Florida Cogeneration Facility-
Westinghouse 501F, Dry Low NOx Combustor, Natural Gas, Base Load

Pollutant		Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F
A	B	C	D	E	F	G
Hours of Operation		8460		8460		8460
Antimony (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Barium (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Cobalt (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Zinc (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Chlorine (lb/hr)= Negligible						
Basis, ppm		NA	NA	NA	NA	NA
Natural gas (cf)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA

Table A-19A. Design Information and Stack Parameters for DESTEC Central Florida Cogeneration Facility-
Westinghouse 501F, Conventional Combustor, Distillate Oil, 70 Percent Load

Data		Gas Turbine Fuel Oil 27 °F	* Not Available * Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	* Not Available * Gas Turbine Fuel Oil 79 °F	Gas Turbine Fuel Oil 97 °F	
	A	B	C	D	E	F	G
General							
Power (kW)			133,020.0		113,400.0		102,810.0
Heat Rate (Btu/kwh)			9,770.0		10,310.0		10,680.0
CT Exhaust Flow							
Mass Flow (lb/hr)			2,934,960		2,757,580		2,662,180
Temperature (oF)			1,130		1,130		1,130
Moisture (% Vol.)			10.43		11.58		12.09
Oxygen (% Vol.)			12.08		12.17		12.26
Molecular Weight			28.34		28.19		28.12
Heat Input (MMBtu/hr)= Power (kW) x Heat Rate (Btu/kwh) ÷ 1,000,000 Btu/MMBtu							
Power (kW)			133,020.0		113,400.0		102,810.0
Heat Rate (Btu/kwh)			9,770.0		10,310.0		10,680.0
Heat Input (MMBtu/hr)			1,299.6		1,169.2		1,098.0
Fuel Oil Consumption (lb/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu ÷ Fuel Heat Content, LHV (Btu/lb)							
Heat Input (MMBtu/hr)			1,299.6		1,169.2		1,098.0
Heat Content, LHV (Btu/lb)			18,450		18,450		18,450
Fuel Oil (lb/hr)			70,439.3		63,368.8		59,512.8
Volume Flow (acfm)= [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F)+ 460°F)] ÷ [Molecular weight x 2116.8] ÷ 60 min/hr							
Mass Flow (lb/hr)			2,934,960		2,757,580		2,662,180
Temperature (°F)			1,130		1,130		1,130
Molecular Weight			28.34		28.19		28.12
Volume Flow (acfm)			2,003,120		1,892,217		1,831,107
Volume Flow (scfm)= [(Mass Flow (lb/hr) x 1,545 x (68°F + 460°F)] ÷ [Molecular weight x 2116.8] ÷ 60 min/hr							
Mass Flow (lb/hr)			2,934,960		2,757,580		2,662,180
Temperature (°F)			68		68		68
Molecular Weight			28.34		28.19		28.12
Volume Flow (scfm)			665,187		628,359		608,066
HRSG Stack Data							
Stack Height (ft)			180		180		180
Diameter (ft)			18.0		18.0		18.0
Volume Flow (acfm) from HRSG= [Volume flow (acfm) x (HRSG temp.(°F)+ 460°F)] ÷ [CT temp.(°F)+ 460°F]							
Volume Flow (acfm) from CT			2,003,120		1,892,217		1,831,107
CT Temperature (°F)			1,130		1,130		1,130
HRSG Temperature (°F)			200		200		200
Volume Flow (acfm) from HRSG			831,484		785,449		760,082
Velocity (ft/sec)= Volume flow (acfm) from HRSG ÷ [((diameter)² ÷ 4) x 3.14159] ÷ 60 sec/min							
Volume Flow (acfm) from HRSG			831,484		785,449		760,082
Diameter (ft)			18.0		18.0		18.0
Velocity (ft/sec)			54.5		51.4		49.8

Note: Universal gas constant= 1,545 ft-lb(force)/°R; atmospheric pressure= 2,116.8 lb(force)/ft²

Source: Westinghouse, 1992.

Table A-20A. Maximum Emissions for Criteria Pollutants for DESTEC Central Florida Cogeneration Facility-
Westinghouse 501F, Conventional Combustor, Distillate Oil, 70 Percent Load

Pollutant	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F	
	Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F		
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Particulate (lb/hr)= Emission rate (lb/hr) from manufacturer						
Basis, lb/hr (manufactur.) (1)		32.6		30.0		28.5
lb/hr		32.6		30.0		28.5
TPY		4.9		4.5		4.3
Sulfur Dioxide (lb/hr)= Fuel oil (lb/hr) x sulfur content(fraction) x (lb SO2/lb S) x fraction emitted as SO2						
Fuel Oil (lb/hr)		70,439.3		63,368.8		59,512.8
Sulfur content (%)		0.05		0.05		0.05
lb SO2/lb S (64/32)		2.0		2.0		2.0
SO2 Fraction emitted		1.00		1.00		1.00
lb/hr		72.69		65.65		61.77
TPY		10.9		9.8		9.3
Nitrogen Oxides (lb/hr)= NOx(ppm) x [(20.9 x (1 - Moisture(%)/100)) - Oxygen(%)] x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		42.5		42.5		42.7
Moisture (%)		10.43		11.58		12.09
Oxygen (%)		12.08		12.17		12.26
Volume Flow (acfm)		2,003,120		1,892,217		1,831,107
Temperature (°F)		1130		1130		1130
lb/hr		227.9		204.5		192.7
TPY		34.2		30.7		28.9
Carbon Monoxide (lb/hr)= CO(ppm) x [1 - Moisture(%)/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm+ (1)		51.5		51.5		51.5
Moisture (%)		10.43		11.58		12.09
Volume Flow (acfm)		2,003,120		1,892,217		1,831,107
Temperature (°F)		1130		1130		1130
lb/hr		133.8		124.7		120.0
TPY		20.1		18.7		18.0
VOCs (lb/hr)= VOC(ppm) x [1 - Moisture(%)/100] x 2116.8 lb/ft2 x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm+ (1)		10.0		10.1		10.5
Moisture (%)		10.43		11.58		12.09
Volume Flow (acfm)		2,003,120		1,892,217		1,831,107
Temperature (°F)		1130		1130		1130
lb/hr		14.84		13.98		13.98
TPY		2.2		2.1		2.1
Lead (lb/hr)= Lead (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (2)		8.9		8.9		8.9
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		1.16E-02		1.04E-02		9.77E-03
TPY		1.73E-03		1.56E-03		1.47E-03

* corrected to 15% O2 dry conditions
+ corrected to dry conditions

Source: (1) Westinghouse, 1992; (2) EPA, 1990

Table A-21A. Maximum Emissions of Other Regulated Pollutants for DESTEC Central Florida Cogeneration Facility Westinghouse 501F, Conventional Combustor, Distillate Oil, 70 Percent Load

Pollutant	Units	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F
		Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F	
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Arsenic (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		4.2		4.2		4.2
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		5.46E-03		4.91E-03		4.61E-03
TPY		8.19E-04		7.37E-04		6.92E-04
Beryllium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		2.5		2.5		2.5
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		3.25E-03		2.92E-03		2.75E-03
TPY		4.87E-04		4.38E-04		4.12E-04
Mercury (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		3		3		3
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		3.90E-03		3.51E-03		3.29E-03
TPY		5.85E-04		5.26E-04		4.94E-04
Fluoride (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (2)		14		14		14
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		4.23E-02		3.80E-02		3.57E-02
TPY		6.34E-03		5.71E-03		5.36E-03
Sulfuric Acid Mist (lb/hr) = Fraction of SO2 Emission Rate x SO2 Emission Rate x lb H2SO4/lb SO2						
Fraction SO2 (%)		8		8		8
SO2 (lb/hr)		72.7		65.7		61.8
lb H2SO4/lb SO2 (98/64)		1.53		1.53		1.53
lb/hr		8.90E+00		8.04E+00		7.57E+00
TPY		1.34E+00		1.21E+00		1.14E+00

Note: Multiply by 2.324 to convert picogram/Joule (pg/J) to lb/10E+12 Btu.

Sources: (1) EPA, 1990; (2) EPA, 1980

Table A-22A. Maximum Emissions of Non-Regulated Pollutants for DESTEC Central Florida Cogeneration Facility-
Westinghouse 501F, Conventional Combustor, Distillate Oil, 70 Percent Load

Pollutant	Units	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F
		Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F	
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Manganese (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		14		14		14
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		1.82E-02		1.64E-02		1.54E-02
TPY		2.73E-03		2.46E-03		2.31E-03
Nickel (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		170		170		170
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		2.21E-01		1.99E-01		1.87E-01
TPY		3.31E-02		2.98E-02		2.80E-02
Cadmium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		10.5		10.5		10.5
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		1.36E-02		1.23E-02		1.15E-02
TPY		2.05E-03		1.84E-03		1.73E-03
Chromium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		47.5		47.5		47.5
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		6.17E-02		5.55E-02		5.22E-02
TPY		9.26E-03		8.33E-03		7.82E-03
Copper (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		280		280		280
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		3.64E-01		3.27E-01		3.07E-01
TPY		5.46E-02		4.91E-02		4.61E-02
Vanadium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		69.5		69.5		69.5
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		9.03E-02		8.13E-02		7.63E-02
TPY		1.35E-02		1.22E-02		1.14E-02
Selenium (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		23.42		23.42		23.42
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		3.04E-02		2.74E-02		2.57E-02
TPY		4.57E-03		4.11E-03		3.86E-03
Polycyclic Organic Matter (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		0.278		0.278		0.278
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		3.61E-04		3.25E-04		3.05E-04
TPY		5.42E-05		4.88E-05		4.58E-05
Formaldehyde (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		405		405		405
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		5.26E-01		4.74E-01		4.45E-01
TPY		7.90E-02		7.10E-02		6.67E-02

Source: (1) EPA, 1990

Table A-23A. Maximum Emissions for Additional Non-Regulated Pollutant for DESTEC Central Florida Cogeneration Facility- Westinghouse 501F, Conventional Combustor, Distillate Oil, 70 Percent Load

Pollutant	* Not Available *		* Not Available *		Gas Turbine Fuel Oil 97 °F	
	Gas Turbine Fuel Oil 27 °F	Gas Turbine Fuel Oil 64 °F	Gas Turbine Fuel Oil 72 °F	Gas Turbine Fuel Oil 79 °F		
A	B	C	D	E	F	G
Hours of Operation		300		300		300
Antimony (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		9.4		9.4		9.4
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		2.84E-02		2.55E-02		2.40E-02
TPY		4.26E-03		3.83E-03		3.60E-03
Barium (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		8.4		8.4		8.4
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		2.54E-02		2.28E-02		2.14E-02
TPY		3.81E-03		3.42E-03		3.22E-03
Cobalt (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		3.9		3.9		3.9
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		1.18E-02		1.06E-02		9.95E-03
TPY		1.77E-03		1.59E-03		1.49E-03
Zinc (lb/hr)= Basis (pg/J) x 2.324 x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, pg/J (1)		294		294		294
HIR (MMBtu/hr)		1,299.6		1,169.2		1,098.0
lb/hr		8.88E-01		7.99E-01		7.50E-01
TPY		1.33E-01		1.20E-01		1.13E-01
Chlorine (lb/hr)= Basis (ppm) x Fuel oil (lb/hr) ÷ 1,000,000 (adj. for ppm)						
Basis, ppm		0.5		0.5		0.5
Fuel Oil (lb/hr)		70,439.3		63,368.8		59,512.8
lb/hr		3.52E-02		3.17E-02		2.98E-02
TPY		5.28E-03		4.75E-03		4.46E-03

Note: Multiply by 2.324 to convert picogram/Joule (pg/J) to lb/10E+12 Btu.

Source: (1) EPA, 1979

Table A-24A. Design Information and Stack Parameters for DESTEC Central Florida Cogeneration Facility-
Westinghouse 501F, Dry Low NOx Combustor, Natural Gas, 70 Percent Load

Data	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F	
A	B	C	D	E	F	G
General						
Power (kW)	118,330.0	103,390.0	100,210.0	97,490.0	90,340.0	
Heat Rate (Btu/kwh)	10,490.0	11,020.0	11,150.0	11,270.0	11,600.0	
CT Exhaust Flow						
Mass Flow (lb/hr)	2,754,000	2,678,720	2,647,790	2,619,850	2,554,960	
Temperature (oF)	1,130	1,130	1,130	1,130	1,130	
Moisture (% Vol.)	7.30	8.32	8.68	9.12	9.29	
Oxygen (% Vol.)	13.04	13.10	13.08	13.04	13.15	
Molecular Weight	28.49	28.36	28.33	28.27	28.25	
Heat Input (MMBtu/hr)= Power (kW) x Heat Rate (Btu/kwh) ÷ 1,000,000 Btu/MMBtu						
Power (kW)	118,330.0	103,390.0	100,210.0	97,490.0	90,340.0	
Heat Rate (Btu/kwh)	10,490.0	11,020.0	11,150.0	11,270.0	11,600.0	
Heat Input (MMBtu/hr)	1,241.3	1,139.4	1,117.3	1,098.7	1,047.9	
Natural Gas Consumption (lb/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu ÷ Fuel Heat Content, LHV (Btu/lb) (cf/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu ÷ Fuel Heat Content, LHV (Btu/cf)						
Heat Input (MMBtu/hr)	1,241.3	1,139.4	1,117.3	1,098.7	1,047.9	
Heat Content, LHV (Btu/lb)	20,900	20,900	20,900	20,900	20,900	
Natural Gas (lb/hr)	59,391.5	54,514.7	53,461.3	52,570.0	50,140.9	
Heat Content, LHV (Btu/cf)	950	950	950	950	950	
Natural Gas (cf/hr)	1,306,612	1,199,324	1,176,149	1,156,539	1,103,099	
Volume Flow (acfm)= [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F)+ 460°F)] ÷ [Molecular weight x 2116.8] + 60 min/hr						
Mass Flow (lb/hr)	2,754,000	2,678,720	2,647,790	2,619,850	2,554,960	
Temperature (°F)	1,130	1,130	1,130	1,130	1,130	
Molecular Weight	28.49	28.36	28.33	28.27	28.25	
Volume Flow (acfm)	1,869,744	1,826,635	1,807,837	1,792,201	1,749,383	
Volume Flow (scfm)= [(Mass Flow (lb/hr) x 1,545 x (68°F + 460°F)] ÷ [Molecular weight x 2116.8] + 60 min/hr						
Mass Flow (lb/hr)	2,754,000	2,678,720	2,647,790	2,619,850	2,554,960	
Temperature (°F)	68	68	68	68	68	
Molecular Weight	28.49	28.36	28.33	28.27	28.25	
Volume Flow (scfm)	620,896	606,581	600,338	595,146	580,927	
HRSG Stack Data						
Stack Height (ft)	180	180	180	180	180	
Diameter (ft)	18.0	18.0	18.0	18.0	18.0	
Volume Flow (acfm) from HRSG= [Volume flow (acfm) x (HRSG temp.(°F)+ 460°F)] ÷ [CT temp.(°F)+ 460°F]						
Volume Flow (acfm) from CT	1,869,744	1,826,635	1,807,837	1,792,201	1,749,383	
CT Temperature (°F)	1,130	1,130	1,130	1,130	1,130	
HRSG Temperature (°F)	200	200	200	200	200	
Volume Flow (acfm) from HRSG	776,120	758,226	750,423	743,932	726,159	
Velocity (ft/sec)= Volume flow (acfm) from HRSG ÷ [(diameter)²+ 4) x 3.14159] ÷ 60 sec/min						
Volume Flow (acfm) from HRSG	776,120	758,226	750,423	743,932	726,159	
Diameter (ft)	18.0	18.0	18.0	18.0	18.0	
Velocity (ft/sec)	50.8	49.7	49.1	48.7	47.6	

Note: Universal gas constant= 1,545 ft-lb(force)/°R; atmospheric pressure= 2,116.8 lb(force)/ft²

Source: Westinghouse, 1992.

Table A-25A. Maximum Emissions for Criteria Pollutants for DESTEC Central Florida Cogeneration Facility-
Westinghouse 501F, Dry Low NOx Combustor, Natural Gas, 70 Percent Load

Pollutant	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F	
A	B	C	D	E	F	G
Hours of Operation		8460	8460	8460	8460	8460
Particulate (lb/hr)= Emission rate (lb/hr) from manufacturer						
Basis, lb/hr (manufactur.) (1)		4.90	4.80	4.70	4.70	4.60
lb/hr		4.90	4.80	4.70	4.70	4.60
TPY		20.73	20.30	19.88	19.88	19.46
Sulfur Dioxide (lb/hr)= Natural gas (cf/hr) x sulfur content(gr/100 cf) x 1 lb/7000 gr x (lb SO2/lb S) + 100						
Natural Gas (cf/hr)		1,306,612	1,199,324	1,176,149	1,156,539	1,103,099
Basis, gr/100 cf		1.0	1.0	1.0	1.0	1.0
lb SO2/lb S (64/32)		2.0	2.0	2.0	2.0	2.0
lb/hr		3.73	3.43	3.36	3.30	3.15
TPY		15.79	14.49	14.21	13.98	13.33
Nitrogen Oxides (lb/hr)= NOx(ppm) x [(20.9 x (1 - Moisture%)/100)] - Oxygen(%) x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		25.4	25.4	25.4	25.4	25.4
Moisture (%)		7.3	8.32	8.68	9.12	9.29
Oxygen (%)		13.04	13.1	13.08	13.04	13.15
Volume Flow (acfm)		1,869,744	1,826,635	1,807,837	1,792,201	1,749,383
Temperature (°F)		1130	1130	1130	1130	1130
lb/hr		121.3	113.4	111.2	109.3	104.0
TPY		512.94	479.50	470.24	462.14	440.07
Carbon Monoxide (lb/hr)= CO(ppm) x [1 - Moisture%]/100 x 2116.8 lb/ft2 x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		10.4	10.3	10.4	10.2	10.4
Moisture (%)		7.3	8.32	8.68	9.12	9.29
Volume Flow (acfm)		1,869,744	1,826,635	1,807,837	1,792,201	1,749,383
Temperature (°F)		1130	1130	1130	1130	1130
lb/hr		26.1	25.0	24.9	24.1	23.9
TPY		110.38	105.63	105.44	101.73	101.06
VOCs (lb/hr)= VOC(ppm) x [1 - Moisture%]/100 x 2116.8 lb/ft2 x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr ÷ [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]						
Basis, ppm* (1)		4.2	4.3	4.4	4.5	3.8
Moisture (%)		7.3	8.32	8.68	9.12	9.29
Volume Flow (acfm)		1,869,744	1,826,635	1,807,837	1,792,201	1,749,383
Temperature (°F)		1130	1130	1130	1130	1130
lb/hr		6.02	5.96	6.01	6.06	4.99
TPY		25.47	25.20	25.42	25.65	21.10
Lead (lb/hr)= Negligible						
Basis, lb/10E+12 Btu		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA

* corrected to 15% O2 dry conditions
+ corrected to dry conditions

Source: Westinghouse, 1992.

Table A-26A. Maximum Emissions of Other Regulated Pollutants for DESTEC Central Florida Cogeneration Facility Westinghouse 501F, Dry Low NOx Combustor, Natural Gas, 70 Percent Load

Pollutant	Units	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F
A	B	C	D	E	F	G
Hours of Operation		8460	8460	8460	8460	8460
Arsenic (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Beryllium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Mercury (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Fluoride (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Sulfuric Acid Mist (lb/hr) = Fraction of SO2 Emission Rate x SO2 Emission Rate x lb H2SO4/lb SO2						
Fraction SO2 (%)		8	8	8	8	8
SO2 (lb/hr)		3.73	3.43	3.36	3.30	3.15
lb H2SO4/lb SO2 (98/64)		1.53	1.53	1.53	1.53	1.53
lb/hr		4.81E-01	4.42E-01	4.33E-01	4.26E-01	4.06E-01
TPY		2.04E+00	1.87E+00	1.83E+00	1.80E+00	1.72E+00

Source: (1) EPA, 1990

Table A-27A. Maximum Emissions of Non-Regulated Pollutants for DESTEC Central Florida Cogeneration Facility-
Westinghouse 501F, Dry Low NOx Combustor, Natural Gas, 70 Percent Load

Pollutant	Units	Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F
A	B	C	D	E	F	G
Hours of Operation		8460	8460	8460	8460	8460
Manganese (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Nickel (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Cadmium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Chromium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Copper (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Vanadium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Selenium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Polycyclic Organic Matter (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		1.113	1.113	1.113	1.113	1.113
HIR (MMBtu/hr)		1,241.3	1,139.4	1,117.3	1,098.7	1,047.9
lb/hr		1.38E-03	1.27E-03	1.24E-03	1.22E-03	1.17E-03
TPY		5.84E-03	5.36E-03	5.26E-03	5.17E-03	4.93E-03
Formaldehyde (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		88.12	88.12	88.12	88.12	88.12
HIR (MMBtu/hr)		1,241.3	1,139.4	1,117.3	1,098.7	1,047.9
lb/hr		1.09E-01	1.00E-01	9.85E-02	9.68E-02	9.23E-02
TPY		4.63E-01	4.25E-01	4.16E-01	4.10E-01	3.91E-01

Source: (1) EPA, 1990

Table A-28A. Maximum Emissions for Additional Non-Regulated Pollutant for DESTEC Central Florida Cogeneration Facility-
Westinghouse 501F, Dry Low NOx Combustor, Natural Gas, 70 Percent Load

Pollutant		Gas Turbine Natural Gas 27 °F	Gas Turbine Natural Gas 64 °F	Gas Turbine Natural Gas 72 °F	Gas Turbine Natural Gas 79 °F	Gas Turbine Natural Gas 97 °F
A	B	C	D	E	F	G
Hours of Operation		8460		8460		8460
Antimony (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Barium (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Cobalt (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Zinc (lb/hr)= Negligible						
Basis, pg/J		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Chlorine (lb/hr)= Negligible						
Basis, ppm		NA	NA	NA	NA	NA
Natural gas (cf)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA

Table A-11. Design Information for DESTEC Central Florida Cogeneration Facility-
Duct Burner, Supplemental Firing, Natural Gas

Data		Natural Gas 27 °F	Natural Gas 64 °F	Natural Gas 72 °F	Natural Gas 79 °F	Natural Gas 97 °F
A	B	C	D	E	F	G
General						
Power (kW)		NA	NA	NA	NA	NA
Heat Rate (Btu/kwh)		NA	NA	NA	NA	NA
DB Exhaust Flow						
Mass Flow (lb/hr)		5,244	5,244	5,244	5,244	5,244
Temperature (oF)		205	205	205	205	205
Moisture (% Vol.)		NA	NA	NA	NA	NA
Oxygen (% Vol.)		NA	NA	NA	NA	NA
Molecular Weight		28.00	28.00	28.00	28.00	28.00
Heat Input (MMBtu/hr)= As given						
Power (kW)		NA	NA	NA	NA	NA
Heat Rate (Btu/kwh)		NA	NA	NA	NA	NA
Heat Input (MMBtu/hr)		100.0	100.0	100.0	100.0	100.0
Natural Gas Consumption (lb/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu + Fuel Heat Content, LHV (Btu/lb) (cf/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu + Fuel Heat Content, LHV (Btu/cf)						
Heat Input (MMBtu/hr)		100.0	100.0	100.0	100.0	100.0
Heat Content, LHV (Btu/lb)		23,839	23,839	23,839	23,839	23,839
Natural Gas (lb/hr)		4,194.8	4,194.8	4,194.8	4,194.8	4,194.8
Heat Content, LHV (Btu/cf)		950	950	950	950	950
Natural Gas (cf/hr)		105,263	105,263	105,263	105,263	105,263
Volume Flow (acfm)= [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F)+ 460°F)] ÷ [Molecular weight x 2116.8] + 60 min/hr						
Mass Flow (lb/hr)		5,244	5,244	5,244	5,244	5,244
Temperature (°F)		205	205	205	205	205
Molecular Weight		28.00	28.00	28.00	28.00	28.00
Volume Flow (acfm)		1,515	1,515	1,515	1,515	1,515
Volume Flow (scfm)= [(Mass Flow (lb/hr) x 1,545 x (68°F + 460°F)] ÷ [Molecular weight x 2116.8] + 60 min/hr						
Mass Flow (lb/hr)		5,244	5,244	5,244	5,244	5,244
Temperature (°F)		68	68	68	68	68
Molecular Weight		28.00	28.00	28.00	28.00	28.00
Volume Flow (scfm)		1,203	1,203	1,203	1,203	1,203
HRSG Stack Data						
Stack Height (ft)		180	180	180	180	180
Diameter (ft)		18.0	18.0	18.0	18.0	18.0
Volume Flow (acfm) from DB= [Volume flow (acfm) x (HRSG temp.(°F)+ 460°F)] ÷ [CT temp.(°F)+ 460°F]						
Volume Flow (acfm) from DB		1,515	1,515	1,515	1,515	1,515
Assumed DB Exhaust Temp.(°F)		205	205	205	205	205
HRSG Temperature (°F)		205	205	205	205	205
Volume Flow (acfm) from DB		1,515	1,515	1,515	1,515	1,515
Velocity (ft/sec)= Volume flow (acfm) from DB ÷ [((diameter)²+ 4) x 3.14159] ÷ 60 sec/min						
Volume Flow (acfm) from DB		1,515	1,515	1,515	1,515	1,515
Diameter (ft)		18.0	18.0	18.0	18.0	18.0
Velocity (ft/sec)		0.1	0.1	0.1	0.1	0.1

Note: Universal gas constant= 1,545 ft-lb(force)/°R; atmospheric pressure= 2,116.8 lb(force)/ft²

Source: Destec Engineering, Inc., 1992

Table A-12. Maximum Emissions for Criteria Pollutants for DESTEC Central Florida Cogeneration Facility-Duct Burner, Supplemental Firing, Natural Gas

Pollutant		Natural Gas 27 °F	Natural Gas 64 °F	Natural Gas 72 °F	Natural Gas 79 °F	Natural Gas 97 °F
A	B	C	D	E	F	G
Hours of Operation		8760	8760	8760	8760	8760
Particulate (lb/hr)= Basis (lb/MMBtu) x HIR (MMBtu/hr)						
Basis, lb/MMBtu		0.01	0.01	0.01	0.01	0.01
HIR, MMBtu/hr		100.0	100.0	100.0	100.0	100.0
lb/hr		1.00	1.00	1.00	1.00	1.00
TPY		4.38	4.38	4.38	4.38	4.38
Sulfur Dioxide (lb/hr)= Natural gas (cf/hr) x sulfur content(gr/100 cf) x 1 lb/7000 gr x (lb SO2/lb S) + 100						
Natural Gas (cf/hr)		105,263	105,263	105,263	105,263	105,263
Basis, gr/100 cf		1.0	1.0	1.0	1.0	1.0
lb SO2/lb S (64/32)		2.0	2.0	2.0	2.0	2.0
lb/hr		0.30	0.30	0.30	0.30	0.30
TPY		1.32	1.32	1.32	1.32	1.32
Nitrogen Oxides (lb/hr)= Basis (lb/MMBtu/hr) x HIR (MMBtu/hr)						
Basis, lb/MMBtu		0.10	0.10	0.10	0.10	0.10
HIR, MMBtu/hr		100.0	100.0	100.0	100.0	100.0
lb/hr		10.00	10.00	10.00	10.00	10.00
TPY		43.80	43.80	43.80	43.80	43.80
Carbon Monoxide (lb/hr)= Basis (lb/MMBtu) x HIR (MMBtu/hr)						
Basis, lb/MMBtu		0.10	0.10	0.10	0.10	0.10
HIR, MMBtu/hr		100.0	100.0	100.0	100.0	100.0
lb/hr		10.00	10.00	10.00	10.00	10.00
TPY		43.80	43.80	43.80	43.80	43.80
VOCs (lb/hr)= Basis (lb/MMBtu) x HIR (MMBtu/hr)						
Basis, lb/MMBtu		0.029	0.029	0.029	0.029	0.029
HIR, MMBtu/hr		100.0	100.0	100.0	100.0	100.0
lb/hr		2.90	2.90	2.90	2.90	2.90
TPY		12.70	12.70	12.70	12.70	12.70
Lead (lb/hr)= Negligible						
Basis, lb/MMBtu		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA

Table A-13. Maximum Emissions of Other Regulated Pollutants for DESTEC Central Florida Cogeneration Facility Duct Burner, Supplemental Firing, Natural Gas

Pollutant	Units	Natural Gas	Natural Gas	Natural Gas	Natural Gas	Natural Gas
		27 °F	64 °F	72 °F	79 °F	97 °F
A	B	C	D	E	F	G
Hours of Operation		8760	8760	8760	8760	8760
Arsenic (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Beryllium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Mercury (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Fluoride (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Sulfuric Acid Mist (lb/hr) = Fraction of SO2 Emission Rate x SO2 Emission Rate x lb H2SO4/lb SO2						
Fraction SO2 (%)		8	8	8	8	8
SO2 (lb/hr)		0.30	0.30	0.30	0.30	0.30
lb H2SO4/lb SO2 (98/64)		1.53	1.53	1.53	1.53	1.53
lb/hr		3.68E-02	3.68E-02	3.68E-02	3.68E-02	3.68E-02
TPY		1.61E-01	1.61E-01	1.61E-01	1.61E-01	1.61E-01

Source: EPA, 1990

Table A-14. Maximum Emissions of Non-Regulated Pollutants for DESTEC Central Florida Cogeneration Facility-
Duct Burner, Supplemental Firing, Natural Gas

Pollutant	Units	Natural Gas	Natural Gas	Natural Gas	Natural Gas	Natural Gas
		27 °F	64 °F	72 °F	79 °F	97 °F
A	B	C	D	E	F	G
Hours of Operation		8760	8760	8760	8760	8760
Manganese (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Nickel (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Cadmium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Chromium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Copper (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Vanadium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Selenium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Polycyclic Organic Matter (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		1.113	1.113	1.113	1.113	1.113
HIR (MMBtu/hr)		100.0	100.0	100.0	100.0	100.0
lb/hr		1.11E-04	1.11E-04	1.11E-04	1.11E-04	1.11E-04
TPY		4.87E-04	4.87E-04	4.87E-04	4.87E-04	4.87E-04
Formaldehyde (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) + 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		88.12	88.12	88.12	88.12	88.12
HIR (MMBtu/hr)		100.0	100.0	100.0	100.0	100.0
lb/hr		8.81E-03	8.81E-03	8.81E-03	8.81E-03	8.81E-03
TPY		3.86E-02	3.86E-02	3.86E-02	3.86E-02	3.86E-02

Source: (1) EPA, 1990

Table A-11A. Design Information for DESTEC Central Florida Cogeneration Facility-
Duct Burner, Supplemental Firing, Natural Gas

Data		Natural Gas 27 °F	Natural Gas 64 °F	Natural Gas 72 °F	Natural Gas 79 °F	Natural Gas 97 °F
A	B	C	D	E	F	G
General						
Power (kW)		NA	NA	NA	NA	NA
Heat Rate (Btu/kwh)		NA	NA	NA	NA	NA
DB Exhaust Flow						
Mass Flow (lb/hr)		5,244	5,244	5,244	5,244	5,244
Temperature (of)		200	200	200	200	200
Moisture (% Vol.)		NA	NA	NA	NA	NA
Oxygen (% Vol.)		NA	NA	NA	NA	NA
Molecular Weight		28.00	28.00	28.00	28.00	28.00
Heat Input (MMBtu/hr)= As given						
Power (kW)		NA	NA	NA	NA	NA
Heat Rate (Btu/kwh)		NA	NA	NA	NA	NA
Heat Input (MMBtu/hr)		100.0	100.0	100.0	100.0	100.0
Natural Gas Consumption (lb/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu + Fuel Heat Content, LHV (Btu/lb) (cf/hr)= Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu + Fuel Heat Content, LHV (Btu/cf)						
Heat Input (MMBtu/hr)		100.0	100.0	100.0	100.0	100.0
Heat Content, LHV (Btu/lb)		23,839	23,839	23,839	23,839	23,839
Natural Gas (lb/hr)		4,194.8	4,194.8	4,194.8	4,194.8	4,194.8
Heat Content, LHV (Btu/cf)		950	950	950	950	950
Natural Gas (cf/hr)		105,263	105,263	105,263	105,263	105,263
Volume Flow (acfm)= [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F)+ 460°F)] ÷ [Molecular weight x 2116.8] + 60 min/hr						
Mass Flow (lb/hr)		5,244	5,244	5,244	5,244	5,244
Temperature (°F)		200	200	200	200	200
Molecular Weight		28.00	28.00	28.00	28.00	28.00
Volume Flow (acfm)		1,504	1,504	1,504	1,504	1,504
Volume Flow (scfm)= [(Mass Flow (lb/hr) x 1,545 x (68°F + 460°F)] + [Molecular weight x 2116.8] ÷ 60 min/hr						
Mass Flow (lb/hr)		5,244	5,244	5,244	5,244	5,244
Temperature (°F)		68	68	68	68	68
Molecular Weight		28.00	28.00	28.00	28.00	28.00
Volume Flow (scfm)		1,203	1,203	1,203	1,203	1,203
HRSR Stack Data						
Stack Height (ft)		180	180	180	180	180
Diameter (ft)		18.0	18.0	18.0	18.0	18.0
Volume Flow (acfm) from DB= [Volume flow (acfm) x (HRSR temp.(°F)+ 460°F)] ÷ [CT temp.(°F)+ 460°F]						
Volume Flow (acfm) from DB		1,504	1,504	1,504	1,504	1,504
Assumed DB Exhaust Temp.(°F)		200	200	200	200	200
HRSR Temperature (°F)		200	200	200	200	200
Volume Flow (acfm) from DB		1,504	1,504	1,504	1,504	1,504
Velocity (ft/sec)= Volume flow (acfm) from DB ÷ [((diameter)²+ 4) x 3.14159] ÷ 60 sec/min						
Volume Flow (acfm) from DB		1,504	1,504	1,504	1,504	1,504
Diameter (ft)		18.0	18.0	18.0	18.0	18.0
Velocity (ft/sec)		0.1	0.1	0.1	0.1	0.1

Note: Universal gas constant= 1,545 ft-lb(force)/°R; atmospheric pressure= 2,116.8 lb(force)/ft²

Source: Destec Engineering, Inc., 1992

Table A-13A. Maximum Emissions of Other Regulated Pollutants for DETEC Central Florida Cogeneration Facility
Duct Burner, Supplemental Firing, Natural Gas

Pollutant	Units	Natural Gas	Natural Gas	Natural Gas	Natural Gas	Natural Gas
		27 °F	64 °F	72 °F	79 °F	97 °F
A	B	C	D	E	F	G
Hours of Operation		8760	8760	8760	8760	8760
Arsenic (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Beryllium (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Mercury (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Fluoride (lb/hr)= Negligible Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Sulfuric Acid Mist (lb/hr) = Fraction of SO2 Emission Rate x SO2 Emission Rate x lb H2SO4/lb SO2						
Fraction SO2 (%)		8	8	8	8	8
SO2 (lb/hr)		0.30	0.30	0.30	0.30	0.30
lb H2SO4/lb SO2 (98/64)		1.53	1.53	1.53	1.53	1.53
lb/hr		3.68E-02	3.68E-02	3.68E-02	3.68E-02	3.68E-02
TPY		1.61E-01	1.61E-01	1.61E-01	1.61E-01	1.61E-01

Source: EPA, 1990

Table A-14A. Maximum Emissions of Non-Regulated Pollutants for DESTEC Central Florida Cogeneration Facility-
Duct Burner, Supplemental Firing, Natural Gas

Pollutant	Units	Natural Gas	Natural Gas	Natural Gas	Natural Gas	Natural Gas
		27 °F	64 °F	72 °F	79 °F	97 °F
A	B	C	D	E	F	G
Hours of Operation		8760	8760	8760	8760	8760
Manganese (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Nickel (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Cadmium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Chromium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Copper (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Vanadium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Selenium (lb/hr)= Negligible						
Basis, lb/10E+12 Btu (1)		NA	NA	NA	NA	NA
HIR (MMBtu/hr)		NA	NA	NA	NA	NA
lb/hr		NA	NA	NA	NA	NA
TPY		NA	NA	NA	NA	NA
Polycyclic Organic Matter (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		1.113	1.113	1.113	1.113	1.113
HIR (MMBtu/hr)		100.0	100.0	100.0	100.0	100.0
lb/hr		1.11E-04	1.11E-04	1.11E-04	1.11E-04	1.11E-04
TPY		4.87E-04	4.87E-04	4.87E-04	4.87E-04	4.87E-04
Formaldehyde (lb/hr)= Basis (lb/10E+12 Btu) x Heat Input Rate (MMBtu/hr) ÷ 1,000,000 MMBtu/10E+12 Btu						
Basis, lb/10E+12 Btu (1)		88.12	88.12	88.12	88.12	88.12
HIR (MMBtu/hr)		100.0	100.0	100.0	100.0	100.0
lb/hr		8.81E-03	8.81E-03	8.81E-03	8.81E-03	8.81E-03
TPY		3.86E-02	3.86E-02	3.86E-02	3.86E-02	3.86E-02

Source: (1) EPA, 1990

GE PG 7221 FA
DISTILLATE OIL
BASE LOAD
27°F

12018C2/APPA-1
06/13/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - 27°F CONDITIONS (BASE LOAD)

(From Table A-1 On Distillate Oil;

All Other Calculations on Spreadsheet are Identical.)

Table A-1: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10^6 Btu/hr):

Power (kW) x Heat Rate (10^6 Btu/kWh)

$$183,700 \times 10,070/10^6 = 1,849.9 \times 10^6 \text{ Btu/hr}$$

Fuel Oil (lb/hr):

Heat Input (10^6 Btu/hr) + Fuel Heat Content (Btu/lb)

$$1,849.9 \times 10^6 + 18,550 = 99,723 \text{ lb/hr}$$

Volume Flow (acfm) - See Note A:

$$V = mRT/PM$$

$$3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ = 2,450,287 \text{ acfm}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of 68°F

$$3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ = 851,152 \text{ scfm}$$

GE PG7221FA
Distillate Oil
Base Load
27°F

12018C2/APPA-2
06/13/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$2,450,287 \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + (1,060^\circ\text{F} + 460^\circ\text{F}) \\ - 1,072,001 \text{ acfm}$$

Velocity (ft/sec):

$$\text{Volume Flow (ft}^3\text{/min)} + \text{Area (ft}^2\text{)} + 60 \text{ sec/min} \\ 1,072,001 \text{ ft}^3\text{/min} + 60 + (18.0^2 + 4 \times 3.14159) \\ - 70.2 \text{ ft/sec}$$

Table A-2:

PM emissions in tons per year

$$17 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton} \\ - 2.6 \text{ ton/yr}$$

SO₂ Emissions--Oil (lb/hr)

$$99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2\text{/lb S} \\ - 99.72 \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$42 \text{ ppm} \times [20.9 \times (1 - 11.59/100) - 10.96] \times 2,116.8 \text{ lb/ft}^2 \\ \times 2,450,287 \text{ ft}^3\text{/min} \\ \times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) \\ \times 5.9 \times 10^6 \text{ (adjust for ppm)}] \\ - 326.2 \text{ lb/hr}$$

GE PG7221 FA
Distillate Oil
Base Load
27°F

12018C2/APPA-3
06/12/92

CO Emissions (lb/hr) - See Note C:

$$30 \text{ ppm} \times (1 - 11.59/100) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28$$

(molecular wgt. of carbon)

$$\times 60 \text{ min/hr} + (1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) \times 10^6)$$
$$- 98.4 \text{ lb/hr}$$

VOC Emissions (lb/hr) - See Note C:

$$\frac{4.0}{3.5} \text{ ppm} \times (1 - 11.59/100) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16$$

(molecular wgt. of methane)

$$\times 60 \text{ min/hr} + (1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) \times 10^6)$$
$$- \frac{7.50}{6.56} \text{ lb/hr}$$

Lead Emissions (lb/hr):

$$8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr} - 1.65 \times 10^{-2} \text{ lb/hr}$$

Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb S} \times \frac{0.08}{0.05}$$

(converted)

$$- 12.2 \text{ lb/hr}$$

Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu}$$

$$- 2.59 \times 10^{-2} \text{ lb/hr}$$

Emission Calculations, Tables A-3 A-4, A-5

Manufacturer/Model: GE PB7221FA
 Fuel Type: Distillate Oil
 Load: Base
 Ambient Temperature: 27°F

- Arsenic: 4.2 lb/10¹² Btu x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 7.77×10⁻³ lb/hr
- Beryllium: 2.5 lb/10¹² Btu x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 4.62×10⁻³ lb/hr
- Mercury: 3.0 lb/10¹² Btu x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 5.55×10⁻³ lb/hr
- Fluoride: 14.0 pg/J x 2.324 lb/10¹² Btu/pg/J x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 6.02×10⁻² lb/hr
- Nickel: 170.0 lb/10¹² Btu x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.314 lb/hr
- Cadmium: 10.5 lb/10¹² Btu x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 1.94×10⁻² lb/hr
- Chromium: 47.5 lb/10¹² Btu x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 8.79×10⁻² lb/hr
- Copper: 280 lb/10¹² Btu x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.518 lb/hr
- Vanadium: 69.5 lb/10¹² Btu x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.129 lb/hr
- Selenium: 23.42 lb/10¹² Btu x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 4.33×10⁻² lb/hr
- Polycyclic Organic Matter: 0.278 lb/10¹² Btu x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 5.14×10⁻⁴ lb/hr
- Formaldehyde: 405 lb/10¹² Btu x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.749 lb/hr
- Antimony: 9.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 7.04×10⁻² lb/hr
- Barium: 8.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 3.61×10⁻² lb/hr
- Cobalt: 3.9 pg/J x 2.324 lb/10¹² Btu/pg/J x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 1.68×10⁻² lb/hr
- Zinc: 294 pg/J x 2.324 lb/10¹² Btu/pg/J x 1849.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 1.26 lb/hr
- Chlorine: 0.5 ppm x 99722.9 lb/hr fuel oil + 10⁶ - 4.99×10⁻² lb/hr

GE PG7221 FA
DISTILLATE OIL
BASE LOAD
72 °F

7-29-92

12018G2/APPA-1
06/13/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁷²~~27~~ °F CONDITIONS (BASE LOAD)

(From Table A-1 On Distillate Oil;

All Other Calculations on Spreadsheet are Identical.)

Table A-1: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10⁶ Btu/hr):

Power (kW) x Heat Rate (10⁶ Btu/kWh)

$$\frac{183,700}{159,200} \times \frac{10,070}{10,320} / 10^6 - \frac{1,849.9}{1,642.9} \times 10^6 \text{ Btu/hr}$$

Fuel Oil (lb/hr):

Heat Input (10⁶ Btu/hr) + Fuel Heat Content (Btu/lb)

$$\frac{1,849.9}{1,642.9} \times 10^6 + 18,550 - \frac{99,723}{88,568.4} \text{ lb/hr}$$

Volume Flow (acfm) - See Note A:

$$V = \frac{mRT}{PM}$$

$$\frac{3,743,000}{3,390,000} \text{ lb/hr} \times 1,545 \times \frac{(1,060^\circ\text{F} + 460^\circ\text{F})}{1,102} + \frac{(28.25 \times 2,116.8 \text{ lb/ft}^2)}{28.15}$$

$$+ 60(\text{min/hr})$$

$$- 2,450,287 \text{ acfm}$$

$$2,288,314$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of 68°F

$$\frac{3,743,000}{3,390,000} \text{ lb/hr} \times 1,545 \times \frac{(68^\circ\text{F} + 460^\circ\text{F})}{28.15} + \frac{(28.25 \times 2,116.8)}{28.15} + 60$$

$$- 851,152 \text{ scfm}$$

$$773,514$$

GE P07221FA
 Distillate Oil
 Base Load
 72°F

12018C2/APPA-2
 06/13/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\begin{aligned} & \frac{2,450,287}{2,288,314} \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + \frac{(1,060^\circ\text{F} + 460^\circ\text{F})}{1,102} \\ & - \frac{1,072,001}{974,218} \text{ acfm} \end{aligned}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\begin{aligned} & \frac{1,072,001}{974,218} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159) \\ & - \frac{70.2}{63.8} \text{ ft/sec} \end{aligned}$$

Table A-2:

PM emissions in tons per year

$$17 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$- 2.6 \text{ ton/yr}$$

SO₂ Emissions--Oil (lb/hr)

$$\frac{99,722.9}{88,568.4} \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2/\text{lb S}$$

$$- 99.72 \text{ lb/hr}$$

$$88.57$$

NO_x Emissions (lb/hr) - See Note B:

$$42 \text{ ppm} \times \left[20.9 \times \left(1 - \frac{12.40}{11.59/100} \right) - \frac{10.95}{10.96} \right] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{2,450,287}{2,288,314} \text{ ft}^3/\text{min}$$

$$\times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times \frac{(1,060^\circ\text{F} + 460^\circ\text{F})}{1,102}]$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$- 326.2 \text{ lb/hr}$$

$$290.2$$

GE PG7221 FA
 Distillate Oil
 Base Load
 72°F

12018C2/APPA-3
 06/12/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 30 \text{ ppm} \times (1 - \frac{12.40}{11.59}) / 100 \times \frac{2,288,314}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,102}{1,060} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad \quad \quad 88.6 \\
 & \quad \quad \quad - 98.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 3.9 \text{ ppm} \times (1 - \frac{12.40}{11.59}) / 100 \times \frac{2,288,314}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,102}{1,060} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad \quad \quad 6.58 \\
 & \quad \quad \quad - 6.56 \text{ lb/hr} \\
 & \quad \quad \quad 6.58
 \end{aligned}$$

Lead Emissions (lb/hr):

$$\begin{aligned}
 & 8.9 \text{ lb}/10^{12} \text{ Btu} \times \frac{1,642.9}{1,849.9} \times 10^6 \text{ Btu/hr} - \frac{1.46}{1.65} \times 10^{-2} \text{ lb/hr}
 \end{aligned}$$

Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

$$\begin{aligned}
 & \text{Based on 8 percent of sulfur converted to acid mist} \\
 & \frac{88,568.4}{99,722.9} \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb S} \times \frac{0.08}{0.05} \\
 & \text{(converted)} \\
 & \quad \quad \quad 10.8 \\
 & \quad \quad \quad - 12.2 \text{ lb/hr}
 \end{aligned}$$

Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \frac{1,642.9}{1,849.9} \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu} \\
 & \quad \quad \quad - \frac{2.59}{2.30} \times 10^{-2} \text{ lb/hr} \\
 & \quad \quad \quad 2.30
 \end{aligned}$$

Emission Calculations, Tables A-3, A-4, A-5

Manufacturer/Model: GE PG7221FA
 Fuel Type: Distillate Oil
 Load: Base
 Ambient Temperature: 72°F

- Arsenic: 4.2 lb/10¹² Btu x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 6.9 × 10⁻³ lb/hr
- Beryllium: 2.5 lb/10¹² Btu x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 4.11 × 10⁻³ lb/hr
- Mercury: 3.0 lb/10¹² Btu x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 4.93 × 10⁻³ lb/hr
- Fluoride: 14 pg/J x 2.324 lb/10¹² Btu/pg/J x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 5.35 × 10⁻² lb/hr
- Nickel: 170 lb/10¹² Btu x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.279 lb/hr
- Cadmium: 10.5 lb/10¹² Btu x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 1.73 × 10⁻² lb/hr
- Chromium: 47.5 lb/10¹² Btu x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 7.8 × 10⁻² lb/hr
- Copper: 280 lb/10¹² Btu x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.460 lb/hr
- Vanadium: 69.5 lb/10¹² Btu x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.114 lb/hr
- Selenium: 23.42 lb/10¹² Btu x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.85 × 10⁻² lb/hr
- Polycyclic Organic Matter: 0.278 lb/10¹² Btu x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 4.57 × 10⁻⁴ lb/hr
- Formaldehyde: 405 lb/10¹² Btu x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.665 lb/hr
- Antimony: 9.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 3.59 × 10⁻² lb/hr
- Barium: 8.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 3.21 × 10⁻² lb/hr
- Cobalt: 3.9 pg/J x 2.324 lb/10¹² Btu/pg/J x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 1.49 × 10⁻² lb/hr
- Zinc: 294 pg/J x 2.324 lb/10¹² Btu/pg/J x 1642.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 1.12 lb/hr
- Chlorine: 0.5 ppm x 88568.4 lb/hr fuel oil + 10⁶ - 4.43 × 10⁻² lb/hr

GE PG7221 FA
 DISTILLATE OIL
 BASE LOAD
 97°F

12018G2/APPA-1
 06/13/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT
 EXAMPLE CALCULATIONS - ⁹⁷~~27~~°F CONDITIONS (BASE LOAD)

(From Table A-1 On Distillate Oil;

All Other Calculations on Spreadsheet are Identical.)

Table A-1: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 142,500 \quad 10,650 \quad 1,517.6 \\ \hline 1,837,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Fuel Oil (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,517.6 \quad 81,812.7 \\ \hline 1,849.9 \times 10^6 + 18,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 3,189,000 \quad 1,127 \quad 28.10 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,190,589 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68^\circ\text{F} \\ 3,189,000 \quad 28.10 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ \hline = 851,152 \text{ scfm} \\ 728,816 \end{array}$$

GE PG7221FA
 Distillate Oil
 Base Load
 97°F

12018C2/APPA-2
 06/13/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{2,190,589}{2,450,287} \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + \frac{1,127}{(1,060^\circ\text{F} + 460^\circ\text{F})}$$

$$- 1,072,001 \text{ acfm}$$

$$917,922$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\frac{917,922}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$60.1$$

$$- 70.2 \text{ ft/sec}$$

Table A-2:

PM emissions in tons per year

$$17 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$- 2.6 \text{ ton/yr}$$

SO₂ Emissions--Oil (lb/hr)

$$\frac{81,812.7}{99,722.9} \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2/\text{lb S}$$

$$- 99.72 \text{ lb/hr}$$

$$81.81$$

NO_x Emissions (lb/hr) - See Note B:

$$42 \text{ ppm} \times \left[20.9 \times \left(1 - \frac{12.71}{11.59/100} \right) - 10.96 \right] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{2,190,589}{2,450,287} \text{ ft}^3/\text{min}$$

$$\times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times \frac{1,127}{(1,060^\circ\text{F} + 460^\circ\text{F})}]$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$- 326.2 \text{ lb/hr}$$

$$268.0$$

GE PG7221 FA
Distillate Oil
Base Load
97°F

12018C2/APPA-3
06/12/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned} & 12.71 \quad 2,190,589 \\ & 30 \text{ ppm} \times (1 - \frac{11.59}{100}) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\ & \quad \text{(molecular wgt. of carbon)} \\ & \quad 1,127 \\ & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,127}{1,060} \text{°F} + 460 \text{°F}) \times 10^6) \\ & - 98.4 \text{ lb/hr} \\ & \quad 83.2 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned} & 4.1 \quad 12.71 \quad 2,190,589 \\ & 3.5 \text{ ppm} \times (1 - \frac{11.59}{100}) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\ & \quad \text{(molecular wgt. of methane)} \\ & \quad 1,127 \\ & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,127}{1,060} \text{°F} + 460 \text{°F}) \times 10^6) \\ & - 6.56 \text{ lb/hr} \\ & \quad 6.50 \end{aligned}$$

Lead Emissions (lb/hr):

$$\begin{aligned} & 1,517.6 \quad 1.35 \\ & 8.9 \text{ lb}/10^{12} \text{ Btu} \times \frac{1,517.6}{1,849.9} \times 10^6 \text{ Btu/hr} - 1.65 \times 10^{-2} \text{ lb/hr} \\ & \quad 1.35 \end{aligned}$$

Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

$$\begin{aligned} & \text{Based on 8 percent of sulfur converted to acid mist} \\ & 81,812.7 \quad 0.08 \\ & 99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb S} \times \frac{0.08}{0.05} \\ & \quad \text{(converted)} \\ & - 12.2 \text{ lb/hr} \\ & \quad 10.0 \end{aligned}$$

Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned} & 1,517.6 \\ & \frac{1,517.6}{1,849.9} (\text{MMBtu}) \times 14 \text{ lb}/10^{12} \text{ Btu} \\ & - 2.59 \times 10^{-2} \text{ lb/hr} \\ & \quad 2.12 \end{aligned}$$

Emission Calculations, Tables A-3, A-4, A-5

Manufacturer/Model: GE PG7221FA
 Fuel Type: Distillate Oil
 Load: Base
 Ambient Temperature: 97°F

- Arsenic: 4.2 lb/10¹² Btu x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 6.37 × 10⁻³ lb/hr
- Beryllium: 2.5 lb/10¹² Btu x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.79 × 10⁻³ lb/hr
- Mercury: 3.0 lb/10¹² Btu x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 4.55 × 10⁻³ lb/hr
- Fluoride: 14.0 pg/J x 2.324 lb/10¹² Btu/pg/J x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 4.94 × 10⁻² lb/hr
- Nickel: 170 lb/10¹² Btu x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.258 lb/hr
- Cadmium: 10.5 lb/10¹² Btu x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 1.59 × 10⁻² lb/hr
- Chromium: 47.5 lb/10¹² Btu x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 7.21 × 10⁻² lb/hr
- Copper: 280 lb/10¹² Btu x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.425 lb/hr
- Vanadium: 69.5 lb/10¹² Btu x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.105 lb/hr
- Selenium: 23.42 lb/10¹² Btu x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.55 × 10⁻² lb/hr
- Polycyclic Organic Matter: 0.278 lb/10¹² Btu x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 4.22 × 10⁻⁴ lb/hr
- Formaldehyde: 405 lb/10¹² Btu x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.615 lb/hr
- Antimony: 9.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 3.32 × 10⁻² lb/hr
- Barium: 8.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 2.96 × 10⁻² lb/hr
- Cobalt: 3.9 pg/J x 2.324 lb/10¹² Btu/pg/J x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 1.39 × 10⁻² lb/hr
- Zinc: 294 pg/J x 2.324 lb/10¹² Btu/pg/J x 1517.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 1.04 lb/hr
- Chlorine: 0.5 ppm x 81812.7 lb/hr fuel oil + 10⁶ - 4.09 × 10⁻² lb/hr

GE PG 7221 FA
 NATURAL GAS
 BASE LOAD
 27 °F

12018C2/APPA-1
~~06/22/92~~
 7/29/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - 27°F CONDITIONS

(From Table A-6 On ~~Distillate Oil~~; *Natural Gas*; *Base Load*)

All Other Calculations on Spreadsheet are Identical.)

Table A-6: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 170,700 \quad 9460 \quad 1,614.8 \\ \hline 183,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas
~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,614.8 \quad 21,515 \quad 75,055.6 \\ \hline 1,849.9 \times 10^6 + 18,550 - 99,725 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = \text{mRT/PM} \\ 3,582,000 \quad 1,078 \quad 28.46 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ \text{F} + 460^\circ \text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,354,349 \\ - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68^\circ \text{F} \\ 3,582,000 \quad 28.46 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ \text{F} + 460^\circ \text{F}) + (28.25 \times 2,116.8) + 60 \\ 808,255 \\ - 851,152 \text{ scfm} \end{array}$$

GE PG7221 FA
 Natural Gas
 Base Load
 27°F

12018C2/APPA-2
~~06/29/92~~
 7/29/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$2,354,349 \quad 1,078$$

$$2,450,287 \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + (1,060^\circ\text{F} + 460^\circ\text{F})$$

$$1,017,973$$

$$- 1,072,001 \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$1,017,973$$

$$1,072,001 \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$66.7$$

$$- 70.2 \text{ ft/sec}$$

7
 Table A-2:

PM emissions in tons per year

$$9.0 \quad 8460$$

$$17 \text{ lb/hr} \times 200 \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$39.07$$

$$- 2.6 \text{ ton/yr}$$

Gas
 SO₂ Emissions - Oil (lb/hr)

$$1,699,813 \text{ cf/hr} \quad 1.09 \text{ gr/100cf}$$

$$99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb/7000gr}$$

$$4.86$$

$$= 99.72 \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$25 \quad 7.61 \quad 12.71$$

$$42 \text{ ppm} \times [20.9 \times (1 - \frac{11.59}{100}) - 10.96] \times 2,116.8 \text{ lb/ft}^2$$

$$\times 2,450,287 \text{ ft}^3/\text{min}$$

$$2,354,349$$

$$\times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F})$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}]$$

$$161.9$$

$$- 326.2 \text{ lb/hr}$$

GE PG7221FA
 Natural Gas
 Base Load
 27°F

12018G2/APPA-3
 06/12/92
 7/29/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & \frac{1.5}{3.5} \text{ ppm} \times \left(1 - \frac{7.61}{11.59}\right) \times \frac{2,354,349}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,078}{1,060} \text{°F} + 460 \text{°F}) \times 10^6 \\
 & \quad \frac{48.8}{-98.4} \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & \frac{1.5}{3.5} \text{ ppm} \times \left(1 - \frac{7.61}{11.59}\right) \times \frac{2,354,349}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,078}{1,060} \text{°F} + 460 \text{°F}) \times 10^6 \\
 & \quad \frac{2.79}{-6.56} \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\frac{8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr}}{1.65 \times 10^{-2} \text{ lb/hr}}$$

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 Table A-4:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned}
 & \frac{1,699,813 \text{ cf/hr} \times 1.0 \text{ gr}/100 \text{ cf} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb}/7000 \text{ gr}}{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.66 \text{ lb H}_2\text{SO}_4/\text{lb S}} \times \frac{0.08}{0.05} \times \frac{1.53 \text{ lb H}_2\text{SO}_4}{\text{lb S}} \\
 & \quad \text{(converted)} \\
 & \quad \frac{0.595}{-12.2} \text{ lb/hr}
 \end{aligned}$$

A-8, A-9, A-10
 Tables ~~A-4~~ and ~~A-5~~:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \frac{1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu}}{2.59 \times 10^{-2} \text{ lb/hr}} \quad \text{Not Applicable}
 \end{aligned}$$

7/29/92

Emission Calculations, Tables A-8, A-9, A-10

Manufacturer/Model: GE PG 7221 FA
 Fuel Type: Natural Gas
 Load: Base
 Ambient Temperature: 27°F

Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1614.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 1.8 × 10⁻³ lb/hr

Formaldehyde: 88.12 lb/10¹² Btu x 1614.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.142 lb/hr

Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ - NA lb/hr

'GE PG7221 FA
 NATURAL GAS
 BASE LOAD
 64 °F

12018C2/APPA-1
 06/13/92
 7/29/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁶⁴°F CONDITIONS

(From Table A-6 On ~~Distillate Oil~~; *Natural Gas*; *Base Load*)

All Other Calculations on Spreadsheet are Identical.)

⁶
 Table A-~~6~~: (Note: all other data not calculated but supplied by
 Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 151,900 \quad 9,750 \quad 1,481.0 \\ \hline 1,849,700 \times 10^6 / 10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas
~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,481.0 \quad 21,515 \quad 68,836.9 \\ \hline 1,849.9 \times 10^6 + 10,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 3,322,000 \quad 1,110 \quad 28.33 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (20.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,239,805 \\ \hline - 2,450,207 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of
 68°F

$$\begin{array}{r} 3,322,000 \quad 28.33 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (20.25 \times 2,116.8) + 60 \\ 753,259 \\ \hline = 851,152 \text{ scfm} \end{array}$$

GE PG7221 FA
 Natural Gas
 Base Load
 64°F

12018C2/APPA-2
 66/13/92
 7/29/92

Volume Flow from HRSB (acfm):

CT Exhaust adjusted for temperature

$$\begin{aligned} & 2,239,805 \quad 205 \quad 1,110 \\ & 2,450,287 \text{ acfm} \times \frac{205}{(205^\circ\text{F} + 460^\circ\text{F})} + \frac{1,110}{(1,060^\circ\text{F} + 460^\circ\text{F})} \\ & \quad 948,707 \\ & - 1,072,001 \text{ acfm} \end{aligned}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\begin{aligned} & \frac{948,707}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159) \\ & \quad 62.1 \\ & - 70.2 \text{ ft/sec} \end{aligned}$$

7
 Table A-2:

PM emissions in tons per year

$$\begin{aligned} & 9.0 \quad 8460 \\ & 17 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton} \\ & \quad 38.07 \\ & = 2.6 \text{ ton/yr} \end{aligned}$$

GAS
 SO₂ Emissions - ~~0.11~~ (lb/hr)

$$\begin{aligned} & 1,558,974 \text{ cf/hr} \quad 1.0 \text{ gr}/100 \text{ cf} \\ & 99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb gr/lb} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb}/7000 \text{ gr} \\ & \quad 4.45 \\ & = 99.72 \text{ lb/hr} \end{aligned}$$

NO_x Emissions (lb/hr) - See Note B:

$$\begin{aligned} & 25 \quad 8.83 \quad 12.56 \\ & 42 \text{ ppm} \times [20.9 \times (1 - \frac{8.83}{100}) - 10.96] \times 2,116.8 \text{ lb/ft}^2 \\ & \quad \times \frac{2,450,287}{2,239,805} \text{ ft}^3/\text{min} \\ & \quad \times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times \frac{1,110}{(1,060^\circ\text{F} + 460^\circ\text{F})}] \\ & \quad \times 5.9 \times 10^6 \text{ (adjust for ppm)} \\ & \quad 148.5 \\ & = 126.2 \text{ lb/hr} \end{aligned}$$

GE PG7221 FA
 Natural Gas
 Base Load
 64°F

12018C2/APPA-3
 06/12/92
 7/29/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned} & \frac{15}{50} \text{ ppm} \times \left(1 - \frac{8.83}{11.59}\right) \times \frac{2,239,805}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\ & \quad \text{(molecular wgt. of carbon)} \\ & \times 60 \text{ min/hr} + (1,545 \times \frac{1,110}{1,060} \text{ }^\circ\text{F} + 460^\circ\text{F}) \times 10^6 \\ & \quad - \frac{44.9}{98.4} \text{ lb/hr} \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned} & \frac{1.5}{5.3} \text{ ppm} \times \left(1 - \frac{8.83}{11.59}\right) \times \frac{2,239,805}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\ & \quad \text{(molecular wgt. of methane)} \\ & \times 60 \text{ min/hr} + (1,545 \times \frac{1,110}{1,060} \text{ }^\circ\text{F} + 460^\circ\text{F}) \times 10^6 \\ & \quad - \frac{2.57}{6.56} \text{ lb/hr} \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\frac{8.9 \text{ lb/10}^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr}}{1.65 \times 10^{-2}} \text{ lb/hr}$$

Table A-⁸~~2~~:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\frac{1,558,974 \text{ cf/hr} \times 1.09 \text{ lb/100 cf} \times 2.16 \text{ SO}_2 / 16 \text{ S} \times 1.0 \text{ lb/7000 gr}}{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4 / \text{lb SO}_2 \times 0.05}$$

(converted) 1.53 0.08

$$0.546$$

$$- 12.2 \text{ lb/hr}$$

A-8, A-9, A-10
 Tables ~~A-4 and A-5~~:

EPA emission factor as noted in printout; example for manganese:

$$\frac{1,849.9 \text{ (MMBtu)} \times 14 \text{ lb/10}^{12} \text{ Btu}}{2.59 \times 10^{-2}} \text{ lb/hr}$$

Not Applicable

7/29/92

Emission Calculations, Tables A-8, A-9, A-10

Manufacturer/Model: GE PG7221 FA
Fuel Type: Natural Gas
Load: Base
Ambient Temperature: 64°F

Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1481.0 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= 1.65 x 10⁻³ lb/hr

Formaldehyde: 88.12 lb/10¹² Btu x 1481.0 MMBtu/hr + 10⁶ MMBtu/10¹² Btu = 0.131 lb/hr

Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ = NA lb/hr

GE PG 7221 FA
 NATURAL GAS
 72 °F
 BASE LOAD

12018C2/APPA-1
~~06/13/92~~
 7/30/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁷²°F CONDITIONS

(From Table A-~~3~~⁶ On ~~Distillate Oil~~; *Natural Gas; Base Load*)

All Other Calculations on Spreadsheet are Identical.)

⁶
 Table A-~~3~~⁶: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 147,100 \quad 9860 \quad 1,450.4 \\ \hline 1,837,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas
~~Fuel Oil (lb/hr):~~

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,450.4 \quad 21,615 \quad 67,413.7 \\ \hline 1,849.9 \times 10^6 + 18,550 - 96,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 3,262,000 \quad 1,117 \quad 28.28 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,212,530 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68^\circ\text{F} \\ 3,262,000 \quad 28.28 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 740,784 \\ \hline - 851,152 \text{ scfm} \end{array}$$

GE PG7221 FA
 Natural Gas
 72°F
 Base Load

12018C2/APPA-2
 06/13/92
 7/30/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{2,212,530}{2,450,287} \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + \frac{1,117}{(1,060^\circ\text{F} + 460^\circ\text{F})}$$

$$= 932,995 - 1,072,001 \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\frac{932,995}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$= 61.1 - 70.2 \text{ ft/sec}$$

⁷
 Table A-2:

PM emissions in tons per year

$$\frac{9.0}{17} \text{ lb/hr} \times \frac{8460}{300} \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$= 38.07 - 2.6 \text{ ton/yr}$$

^{GAS}
 SO₂ Emissions--~~0.1~~ (lb/hr)

$$\frac{1,526,743 \text{ cf/hr}}{99,722.9 \text{ lb/hr}} \times \frac{1.0 \text{ gr}}{100 \text{ cf}} \times 2 \text{ lb SO}_2/\text{lb s} \times 1.0 \text{ lb}/7000 \text{ gr}$$

$$= 4.36 - 99.72 \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$\frac{25}{42} \text{ ppm} \times [20.9 \times (1 - \frac{9.21}{11.59/100}) - \frac{12.51}{10.96}] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{2,450,287}{2,212,530} \text{ ft}^3/\text{min}$$

$$\times 46 \text{ (molecular wgt NO}_2) \times 60 \text{ min/hr} + [1.545 \times (1,060^\circ\text{F} + 460^\circ\text{F})]$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$= 145.3 - 326.2 \text{ lb/hr}$$

GE PG7221FA
 Natural Gas
 Base Load
 72°F

12018C2/APPA-3
 06/12/92
 7/30/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & \frac{15}{50} \text{ ppm} \times \left(1 - \frac{9.21}{11.59}\right) \times \frac{2,212,530}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,117}{1,060} \text{ F} + 460 \text{ F}) \times 10^6 \\
 & \quad \frac{44.0}{- 98.4} \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & \frac{1.5}{3.5} \text{ ppm} \times \left(1 - \frac{9.21}{11.59}\right) \times \frac{2,212,530}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,117}{1,060} \text{ F} + 460 \text{ F}) \times 10^6 \\
 & \quad \frac{2.51}{- 6.56} \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\frac{8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr}}{1.65 \times 10^{-2} \text{ lb/hr}}$$

Table A-⁸ 8:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned}
 & \frac{1,526,743 \text{ cf/hr} \times 1.09 \text{ lb}/100 \text{ cf} \times 216 \text{ SO}_2/\text{lb S} \times 1.0 \text{ lb}/7000 \text{ gr}}{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb SO}_2 \times 0.05} \\
 & \quad \text{(converted)} \quad \frac{0.534}{- 12.2} \text{ lb/hr} \quad \frac{0.08}{1.53}
 \end{aligned}$$

Tables A-^{A-8, A-9, A-10} 4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \frac{1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{10} \text{ Btu}}{2.59 \times 10^{-2} \text{ lb/hr}} \quad \text{Not Applicable}
 \end{aligned}$$

Emission Calculations, Tables A-8, A-9, A-10Manufacturer/Model: GE PG 7221 FAFuel Type: NATURAL GASLoad: BASEAmbient Temperature: 72°FArsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrBeryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrMercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrFluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hrNickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrCadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrChromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrCopper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrVanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrSelenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrPolycyclic Organic Matter: 1.113 lb/10¹² Btu x 1450.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= 1.61 x 10⁻³ lb/hrFormaldehyde: 88.12 lb/10¹² Btu x 1450.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu = 0.128 lb/hrAntimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hrBarium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hrCobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hrZinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hrChlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ = NA lb/hr

GE PG 7221 FA
 NATURAL GAS
 79 °F
 BASE LOAD

12018C2/APPA-1
 06/15/92
 7/30/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁷⁹°F CONDITIONS

(From Table A-⁶ On ~~Distillate Oil~~; *Natural Gas, Base Load*)

All Other Calculations on Spreadsheet are Identical.)

⁶
 Table A-⁶ (Note: all other data not calculated but supplied by
 Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 142,700 \quad 9970 \quad 1,422.7 \\ \hline 1,427,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas

~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,422.7 \quad 21,515 \quad 66,126.8 \\ \hline 1,849.9 \times 10^6 + 18,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 3,202,000 \quad 1,124 \quad 28.19 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,188,744 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68^\circ\text{F} \\ 3,202,000 \quad 28.19 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 729,581 \\ \hline - 851,152 \text{ scfm} \end{array}$$

GE PG7221FA
 Natural Gas
 79°F
 Base Load

12018G2/APPA-2
 06/13/92
 7/30/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{2,188,744}{2,450,287} \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + \frac{1,124}{1,060} \text{ acfm} \times (1,060^\circ\text{F} + 460^\circ\text{F})$$

$$= \frac{918,885}{1,072,001} \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\frac{918,885}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$= \frac{60.2}{70.2} \text{ ft/sec}$$

7
 Table A-2:

PM emissions in tons per year

$$\frac{9.0}{17} \text{ lb/hr} \times \frac{8460}{300} \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$= \frac{38.07}{2.6} \text{ ton/yr}$$

Gas

SO₂ Emissions - Oil (lb/hr)

$$\frac{1,497,599 \text{ cf/hr}}{99,722.9 \text{ lb/hr}} \times \frac{1.0 \text{ gr/100 cf}}{0.0005 \text{ lb S/lb}} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb/7000 gr}$$

$$= \frac{4.28}{99.72} \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$\frac{25}{42} \text{ ppm} \times \left[20.9 \times \left(1 - \frac{10.05}{11.59} \right) - \frac{12.36}{10.96} \right] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{2,450,287}{2,188,744} \text{ ft}^3/\text{min}$$

$$\times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + \left[1,545 \times \frac{1,124}{1,060} \times 460^\circ\text{F} \right]$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$= \frac{142.6}{326.2} \text{ lb/hr}$$

PG 7221 FA
 Natural Gas
 Base Load
 79°F

12018C2/APPA-3
 06/12/92
 7/30/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & \frac{15}{30} \text{ ppm} \times (1 - \frac{10.05}{11.59/100}) \times \frac{2,188,744}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,124}{1,060} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad \frac{42.9}{-98.4} \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & \frac{1.6}{3.5} \text{ ppm} \times (1 - \frac{10.05}{11.59/100}) \times \frac{2,188,744}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,124}{1,060} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad \frac{2.62}{-6.56} \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\frac{8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr}}{1.65 \times 10^{-2} \text{ lb/hr}}$$

8
 Table A-9:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\frac{1,497,599 \text{ cp/hr} \times 1.09 \text{ lb}/100 \text{ cp} \times 2.16 \text{ SO}_2/\text{lb S} \times 1.0 \text{ lb}/7000 \text{ gr}}{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times \frac{1.53}{3.06} \text{ lb H}_2\text{SO}_4/\text{lb SO}_2 \times 0.05}$$

0.08

$$\frac{0.524}{-12.2} \text{ lb/hr}$$

A-8, A-9, A-10
 Tables ~~A-4~~ and ~~A-5~~:

EPA emission factor as noted in printout; example for manganese:

$$\frac{1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu}}{2.59 \times 10^{-2} \text{ lb/hr}} \quad \text{Not Applicable}$$

7/30/92

Emission Calculations, Tables A-8, A-9, A-10

Manufacturer/Model: GE PG7221 FA
Fuel Type: Natural Gas
Load: Base
Ambient Temperature: 79°F

- Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1422.7 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- 1.58 × 10⁻³ lb/hr
- Formaldehyde: 88.12 lb/10¹² Btu x 1422.7 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.125 lb/hr
- Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ - NA lb/hr

GE PG 7221 FA
 NATURAL GAS
 BASE LOAD
 97 °F

12018C2/APPA-1
 06/15/92
 7/30/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁹⁷°F CONDITIONS

(From Table A-⁶ On ~~Distillate Oil~~; *Natural Gas*; *Base Load*)

All Other Calculations on Spreadsheet are Identical.)

⁶
 Table A-⁶ (Note: all other data not calculated but supplied by
 Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 131,800 \quad 10,230 \quad 1348.3 \\ \hline 183,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas
~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1348.3 \quad 21,515 \quad 62,668.6 \\ \hline 1,849.9 \times 10^6 + 18,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 3,077,000 \quad 1,140 \quad 28.20 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ \text{F} + 460^\circ \text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,123,643 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68^\circ \text{F} \\ 3,077,000 \quad 28.20 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ \text{F} + 460^\circ \text{F}) + (28.25 \times 2,116.8) + 60 \\ 700,802 \\ \hline - 851,152 \text{ scfm} \end{array}$$

GE PG 7221 FA
 Natural Gas
 Base Load
 97°F

12018G2/APPA-2
 06/15/92
 7/30/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\begin{aligned} & 2,123,643 && 1,140 \\ & \cancel{2,450,287} \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + (\cancel{1,060}^\circ\text{F} + 460^\circ\text{F}) \\ & \quad 882,639 \\ & - \cancel{1,072,001} \text{ acfm} \end{aligned}$$

Velocity (ft/sec):

Volume Flow (ft³/min) ÷ Area (ft²) ÷ 60 sec/min

$$\begin{aligned} & 882,639 \\ & \cancel{1,072,001} \text{ ft}^3/\text{min} \div 60 \div (18.0^2 + 4 \times 3.14159) \\ & \quad 57.8 \\ & - \cancel{70.2} \text{ ft/sec} \end{aligned}$$

7
 Table A-2:

PM emissions in tons per year

9.0 8460

$$\begin{aligned} & \cancel{17} \text{ lb/hr} \times \cancel{300} \text{ hr/yr} + 2,000 \text{ lb/ton} \\ & \quad 38.07 \\ & - \cancel{2.6} \text{ ton/yr} \end{aligned}$$

GAS

SO₂ Emissions - Oil (lb/hr)

1,419,278 cf/hr 1.0 gr/100 cf

$$\begin{aligned} & \cancel{59,722.9} \text{ lb/hr} \times \cancel{0.0005} \text{ lb S/lb} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb}/7000 \text{ gr} \\ & \quad 4.06 \\ & - \cancel{99.72} \text{ lb/hr} \end{aligned}$$

NO_x Emissions (lb/hr) - See Note B:

25 9.91 12.48

$$\begin{aligned} & \cancel{42} \text{ ppm} \times [20.9 \times (1 - \cancel{11.59}/100) - \cancel{10.96}] \times 2,116.8 \text{ lb/ft}^2 \\ & \quad \times \cancel{2,450,287} \text{ ft}^3/\text{min} \\ & \quad \quad 2,123,643 && 1,140 \\ & \times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times (\cancel{1,060}^\circ\text{F} + 460^\circ\text{F}) \\ & \quad \times 5.9 \times 10^6 \text{ (adjust for ppm)}] \\ & \quad 135.0 \\ & - \cancel{326.2} \text{ lb/hr} \end{aligned}$$

BE P07221FA
 Natural Gas
 Base Load
 97°F

12018C2/APPA-3
 06/12/92
 7/30/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 15 \quad 9.91 \quad 2,123,643 \\
 & 50 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,140} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,140}{1,060} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad 41.3 \\
 & = 98.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 1.5 \quad 9.91 \quad 2,123,643 \\
 & 3.5 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,140} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,140}{1,060} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad 2.36 \\
 & = 6.56 \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\cancel{0.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr} = 1.65 \times 10^{-2} \text{ lb/hr}}$$

8
 Table A-8:

H₂SO₄ Mist Emissions (lb/hr):

$$\begin{aligned}
 & \text{Based on 8 percent of sulfur converted to acid mist} \\
 & \underbrace{1,419,278 \text{ cf/hr} \times 1.0 \text{ gr}/100 \text{ cf} \times 216 \text{ SO}_2 / 165 \times 1.0 \text{ lb}/7000 \text{ gr}}_{0.08} \\
 & \sqrt{\frac{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb SO}_2 \times 0.05}{1.53}} \\
 & \quad \text{(converted)} \\
 & \quad 0.497 \\
 & = 12.2 \text{ lb/hr}
 \end{aligned}$$

A-8, A-9, A-10
 Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \cancel{1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu}} \quad \text{Not Applicable} \\
 & \quad \cancel{2.59 \times 10^{-2} \text{ lb/hr}}
 \end{aligned}$$

7/30/92

Emission Calculations, Tables A-8, A-9, A-10

Manufacturer/Model: GE PG7221 FA
 Fuel Type: Natural Gas
 Load: BASE
 Ambient Temperature: 97°F

Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1348.3 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = 1.50 × 10⁻³ lb/hr

Formaldehyde: 88.12 lb/10¹² Btu x 1348.3 MMBtu/hr + 10⁶ MMBtu/10¹² Btu = 0.119 lb/hr

Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ = NA lb/hr

GE PG7221 FA
 DISTILLATE OIL
 70% LOAD
 27 °F

12018C2/APPA-1
 06/13/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - 27°F CONDITIONS (70% LOAD)

(From Table A-1A On Distillate Oil;

All Other Calculations on Spreadsheet are Identical.)

Table A-1A: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 29,200 \quad 11,430 \quad 1,476.8 \\ \hline 183,700 \times 10,070/10^6 = 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Fuel Oil (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,476.8 \quad 79,609.5 \\ \hline 1,849.9 \times 10^6 + 18,550 = 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,837,000 \quad 1,166 \quad 28.23 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 1,988,010 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

$$\begin{array}{r} \text{Same as volume flow (acfm) except adjusted for standard temperature of} \\ 68^\circ\text{F} \\ 2,837,000 \quad 28.23 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ - 851,152 \text{ scfm} \\ 645,553 \end{array}$$

GE PG7221FA
 Distillate Oil
 70% Load
 27°F

12018C2/APPA-2
 06/13/92

Volume Flow from HRSG (acfm):

$$\begin{aligned}
 & \text{CT Exhaust adjusted for temperature} \\
 & 1,988,010 \\
 & 2,450,287 \text{ acfm} \times \left(\frac{200}{205^\circ\text{F} + 460^\circ\text{F}} \right) + \left(\frac{1,166}{1,060^\circ\text{F} + 460^\circ\text{F}} \right) \\
 & - 1,072,001 \text{ acfm} \\
 & \underline{806,941}
 \end{aligned}$$

Velocity (ft/sec):

$$\begin{aligned}
 & \text{Volume Flow (ft}^3\text{/min) + Area (ft}^2\text{) + 60 sec/min} \\
 & 806,941 \\
 & 1,072,001 \text{ ft}^3\text{/min} + 60 + (18.0^2 + 4 \times 3.14159) \\
 & \underline{52.9} \\
 & - 70.2 \text{ ft/sec}
 \end{aligned}$$

Table A-2A:

PM emissions in tons per year

$$\begin{aligned}
 & 17 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton} \\
 & - 2.6 \text{ ton/yr}
 \end{aligned}$$

SO₂ Emissions--Oil (lb/hr)

$$\begin{aligned}
 & 79,609.5 \\
 & 99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2\text{/lb S} \\
 & \underline{79.61} \\
 & - 99.72 \text{ lb/hr}
 \end{aligned}$$

NO_x Emissions (lb/hr) - See Note B:

$$\begin{aligned}
 & 42 \text{ ppm} \times \left[20.9 \times \left(1 - \frac{11.96}{100} \right) - \frac{10.57}{10.96} \right] \times 2,116.8 \text{ lb/ft}^2 \\
 & \times \frac{2,450,287 \text{ ft}^3\text{/min}}{1,988,010} \\
 & \times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + \left[1,545 \times \left(\frac{1,166}{1,060^\circ\text{F} + 460^\circ\text{F}} \right) \right] \\
 & \times 5.9 \times 10^6 \text{ (adjust for ppm)} \\
 & \underline{257.7} \\
 & - 326.2 \text{ lb/hr}
 \end{aligned}$$

GE PG7221 FA
Distillate Oil
70% Lead
27°F

12018C2/APPA-3
06/12/92

CO Emissions (lb/hr) - See Note C:

$$30 \text{ ppm} \times (1 - \frac{11.96}{11.59}) \times \frac{1,988,010}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28$$

(molecular wgt. of carbon)

$$\times 60 \text{ min/hr} + (1,545 \times \frac{1,166}{1,060} \times 10^6)$$
$$= 74.3 - 98.4 \text{ lb/hr}$$

VOC Emissions (lb/hr) - See Note C:

$$3.5 \text{ ppm} \times (1 - \frac{11.96}{11.59}) \times \frac{1,988,010}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16$$

(molecular wgt. of methane)

$$\times 60 \text{ min/hr} + (1,545 \times \frac{1,166}{1,060} \times 10^6)$$
$$= 6.56 - 5.66 \text{ lb/hr}$$

Lead Emissions (lb/hr):

$$8.9 \text{ lb/10}^{12} \text{ Btu} \times \frac{1,476.8}{1,849.9} \times 10^6 \text{ Btu/hr} - \frac{1.31}{1.65} \times 10^{-2} \text{ lb/hr}$$

Table A-3A:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$79,609.5 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb S} \times \frac{0.08}{0.05}$$

(converted)

$$= 12.2 - 9.75 \text{ lb/hr}$$

Tables A-4A and A-5A:

EPA emission factor as noted in printout; example for manganese:

$$\frac{1,476.8}{1,849.9} \text{ (MMBtu)} \times 14 \text{ lb/10}^{12} \text{ Btu}$$

$$= 2.59 - 2.07 \times 10^{-2} \text{ lb/hr}$$

Emission Calculations, Tables A-3A, A-4A, A-5A

Manufacturer/Model: GE PG7221FA
 Fuel Type: Distillate Oil
 Load: 70%
 Ambient Temperature: 27°F

Arsenic: 4.2 lb/10¹² Btu x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 6.2 × 10⁻³ lb/hr

Beryllium: 2.5 lb/10¹² Btu x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.69 × 10⁻³ lb/hr

Mercury: 3.0 lb/10¹² Btu x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 4.43 × 10⁻³ lb/hr

Fluoride: 14.0 pg/J x 2.324 lb/10¹² Btu/pg/J x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 4.8 × 10⁻² lb/hr

Nickel: 170 lb/10¹² Btu x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.251 lb/hr

Cadmium: 10.5 lb/10¹² Btu x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 1.55 × 10⁻² lb/hr

Chromium: 47.5 lb/10¹² Btu x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 7.01 × 10⁻² lb/hr

Copper: 280 lb/10¹² Btu x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.413 lb/hr

Vanadium: 69.5 lb/10¹² Btu x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.103 lb/hr

Selenium: 23.42 lb/10¹² Btu x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.46 × 10⁻² lb/hr

Polycyclic Organic Matter: 0.278 lb/10¹² Btu x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 4.11 × 10⁻⁴ lb/hr

Formaldehyde: 405 lb/10¹² Btu x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.598 lb/hr

Antimony: 9.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 3.23 × 10⁻² lb/hr

Barium: 8.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 2.88 × 10⁻² lb/hr

Cobalt: 3.9 pg/J x 2.324 lb/10¹² Btu/pg/J x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 1.34 × 10⁻² lb/hr

Zinc: 294 pg/J x 2.324 lb/10¹² Btu/pg/J x 1476.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 1.01 lb/hr

Chlorine: 0.5 ppm x 79609.5 lb/hr fuel oil + 10⁶ - 3.98 × 10⁻² lb/hr

GE PG 7221 FA
DISTILLATE OIL
70% LOAD
72°F

12018C2/APPA-1
06/13/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁷²/₂₇°F CONDITIONS (70% LOAD)

(From Table A-1A On Distillate Oil;

All Other Calculations on Spreadsheet are Identical.)

Table A-1A: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 111,000 \quad 11,800 \quad 1,309.8 \\ \hline 1,311,700 \times 10,070/10^6 = 1,319.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Fuel Oil (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,309.8 \quad 70,609.2 \\ \hline 1,319.9 \times 10^6 + 18,550 = 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,619,000 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,192^\circ\text{F} + 460^\circ\text{F}) + (28.16 \\ \hline + 60(\text{min/hr}) \\ 1,869,045 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

$$\begin{array}{r} \text{Same as volume flow (acfm) except adjusted for standard temperature of} \\ 68^\circ\text{F} \\ 2,619,000 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.16 \\ \hline 597,370 \\ \hline - 851,152 \text{ scfm} \end{array}$$

GE PG 7221FA
Distillate Oil
70% Load
72°F

12018C2/APPA-2
06/13/92

Volume Flow from HRSG (acfm):

$$\begin{aligned} & \text{CT Exhaust adjusted for temperature} \\ & \frac{1,869,045}{2,450,287} \text{ acfm} \times \frac{200}{(205^\circ\text{F} + 460^\circ\text{F})} + \frac{1,192}{(1,060^\circ\text{F} + 460^\circ\text{F})} \\ & \quad \underline{746,713} \\ & - 1,072,001 \text{ acfm} \end{aligned}$$

Velocity (ft/sec):

$$\begin{aligned} & \text{Volume Flow (ft}^3\text{/min)} + \text{Area (ft}^2\text{)} + 60 \text{ sec/min} \\ & \frac{746,713}{1,072,001} \text{ ft}^3\text{/min} + 60 + (18.0^2 + 4 \times 3.14159) \\ & \quad \underline{48.9} \\ & - 70.2 \text{ ft/sec} \end{aligned}$$

Table A-2A:

PM emissions in tons per year

$$17 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$= 2.6 \text{ ton/yr}$$

SO₂ Emissions--Oil (lb/hr)

$$\frac{70,609.2}{99,722.9} \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2\text{/lb S}$$

$$\quad \underline{70.61} \\ = 99.72 \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$42 \text{ ppm} \times \left[20.9 \times \left(1 - \frac{12.40}{11.59/100} \right) - 10.81 \right] \times 2,116.8 \text{ lb/ft}^2 \\ \times \frac{1,869,045}{2,450,287} \text{ ft}^3\text{/min}$$

$$\times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times \frac{1,192}{(1,060^\circ\text{F} + 460^\circ\text{F})}] \\ \times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$\quad \underline{228.4} \\ = 326.2 \text{ lb/hr}$$

GE PG7221FA
Distillate Oil
70% Load
72°F

12018C2/APPA-3
06/12/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned} & 30 \text{ ppm} \times \left(1 - \frac{12.40}{11.59}\right) \times \frac{1,869,045}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\ & \quad \text{(molecular wgt. of carbon)} \\ & \times 60 \text{ min/hr} + (1,545 \times \frac{1,192}{1,060} \text{ F} + 460 \text{ F}) \times 10^6 \\ & \quad - 68.4 \\ & \quad - 98.4 \text{ lb/hr} \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned} & 3.5 \text{ ppm} \times \left(1 - \frac{12.40}{11.59}\right) \times \frac{1,869,045}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\ & \quad \text{(molecular wgt. of methane)} \\ & \times 60 \text{ min/hr} + (1,545 \times \frac{1,192}{1,060} \text{ F} + 460 \text{ F}) \times 10^6 \\ & \quad - 5.21 \\ & \quad - 6.56 \text{ lb/hr} \end{aligned}$$

Lead Emissions (lb/hr):

$$8.9 \text{ lb}/10^{12} \text{ Btu} \times \frac{1,309.8}{1,849.9} \times 10^6 \text{ Btu/hr} - \frac{1.17}{1.63} \times 10^{-2} \text{ lb/hr}$$

Table A-3A:

H₂SO₄ Mist Emissions (lb/hr):

$$\begin{aligned} & \text{Based on 8 percent of sulfur converted to acid mist} \\ & \frac{70,609.2}{99,722.9} \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb S} \times \frac{0.08}{0.05} \\ & \quad \text{(converted)} \\ & \quad - 8.65 \\ & \quad - 12.2 \text{ lb/hr} \end{aligned}$$

Tables A-4A and A-5A:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned} & \frac{1,309.8}{1,849.9} \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu} \\ & \quad - \frac{1.83}{2.59} \times 10^{-2} \text{ lb/hr} \end{aligned}$$

Emission Calculations, Tables A-3A, A-4A, A-5A

Manufacturer/Model: PG7221FA
 Fuel Type: Distillate Oil
 Load: 70%
 Ambient Temperature: 72°F

- Arsenic: 4.2 lb/10¹² Btu x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 5.5 × 10⁻³ lb/hr
- Beryllium: 2.5 lb/10¹² Btu x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.27 × 10⁻³ lb/hr
- Mercury: 3.0 lb/10¹² Btu x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.93 × 10⁻³ lb/hr
- Fluoride: 14.0 pg/J x 2.324 lb/10¹² Btu/pg/J x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 4.26 × 10⁻² lb/hr
- Nickel: 170 lb/10¹² Btu x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.223 lb/hr
- Cadmium: 10.5 lb/10¹² Btu x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 1.38 × 10⁻² lb/hr
- Chromium: 47.5 lb/10¹² Btu x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 6.22 × 10⁻² lb/hr
- Copper: 280 lb/10¹² Btu x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.367 lb/hr
- Vanadium: 69.5 lb/10¹² Btu x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 9.1 × 10⁻² lb/hr
- Selenium: 23.42 lb/10¹² Btu x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.07 × 10⁻² lb/hr
- Polycyclic Organic Matter: 0.278 lb/10¹² Btu x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 3.64 × 10⁻⁴ lb/hr
- Formaldehyde: 405 lb/10¹² Btu x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.53 lb/hr
- Antimony: 9.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 2.86 × 10⁻² lb/hr
- Barium: 8.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 2.56 × 10⁻² lb/hr
- Cobalt: 3.9 pg/J x 2.324 lb/10¹² Btu/pg/J x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 1.19 × 10⁻² lb/hr
- Zinc: 294 pg/J x 2.324 lb/10¹² Btu/pg/J x 1309.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 0.895 lb/hr
- Chlorine: 0.5 ppm x 79609.5 lb/hr fuel oil + 10⁶ - 3.53 × 10⁻² lb/hr

GE PG 7221 FA
DISTILLATE OIL
70% LOAD
97°F

12018C2/APPA-1
06/13/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ~~27~~⁹⁷°F CONDITIONS (70% LOAD)

(From Table A-1A On Distillate Oil;

All Other Calculations on Spreadsheet are Identical.)

Table A-1A: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10^6 Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 98,500 \quad 12,280 \quad 1,209.6 \\ \hline 1,834,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Fuel Oil (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,209.6 \quad 65,206.5 \\ \hline 1,849.9 \times 10^6 + 18,550 = 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,510,000 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,200 \text{ } ^\circ\text{F} + 460^\circ\text{F}) + (28.13 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ \hline 1,802,083 \\ - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

$$\begin{array}{r} \text{Same as volume flow (acfm) except adjusted for standard temperature of} \\ 68^\circ\text{F} \\ 2,510,000 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.13 \times 2,116.8) + 60 \\ \hline 573,193 \\ - 851,152 \text{ scfm} \end{array}$$

GE PG7221 FA
 Distillate Oil
 70% Load
 97°F

12018C2/APPA-2
 06/13/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{1,802,083}{2,450,287} \text{ acfm} \times \frac{200}{(205^\circ\text{F} + 460^\circ\text{F})} + \frac{1,200}{(1,060^\circ\text{F} + 460^\circ\text{F})}$$

$$= \frac{1,072,001}{716,491} \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\frac{716,491}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$= \frac{70.2}{46.9} \text{ ft/sec}$$

Table A-2A:

PM emissions in tons per year

$$17 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$= 2.6 \text{ ton/yr}$$

SO₂ Emissions--Oil (lb/hr)

$$\frac{65,206.5}{99,722.9} \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2/\text{lb S}$$

$$= \frac{65.21}{99.72} \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$42 \text{ ppm} \times \left[20.9 \times \left(1 - \frac{12.48}{11.59} \right) - \frac{11.07}{10.96} \right] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{2,450,287}{1,802,083} \text{ ft}^3/\text{min}$$

$$\times 46 \text{ (molecular wgt NO}_2) \times 60 \text{ min/hr} + \left[1,545 \times \frac{1,200}{(1,060^\circ\text{F} + 460^\circ\text{F})} \right]$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$= \frac{211.0}{326.2} \text{ lb/hr}$$

GE PG7221 FA
 Distillate Oil
 70% Load
 97°F

12018C2/APPA-3
 06/12/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 30 \text{ ppm} \times \left(1 - \frac{12.48}{11.59}\right) \times \frac{1,802,083}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,200}{1,060} \text{ F} + 460 \text{ F}) \times 10^6 \\
 & \quad - \frac{65.6}{28.4} \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 3.5 \text{ ppm} \times \left(1 - \frac{12.48}{11.59}\right) \times \frac{1,802,083}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,200}{1,060} \text{ F} + 460 \text{ F}) \times 10^6 \\
 & \quad - \frac{5.12}{6.56} \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr):

$$8.9 \text{ lb}/10^{12} \text{ Btu} \times \frac{1,209.6}{1,849.9} \times 10^6 \text{ Btu/hr} - \frac{1.08}{1.65} \times 10^{-2} \text{ lb/hr}$$

Table A-3A:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned}
 & \frac{65,206.5}{99,722.9} \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb S} \times \frac{0.08}{0.05} \\
 & \quad \text{(converted)} \\
 & \quad - \frac{7.99}{12.2} \text{ lb/hr}
 \end{aligned}$$

Tables A-4A and A-5A:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \frac{1,209.6}{1,849.9} \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu} \\
 & \quad - \frac{1.69 \times 10^{-2}}{2.59 \times 10^{-2}} \text{ lb/hr}
 \end{aligned}$$

Emission Calculations, Tables A-3A, A-4A, A-5A

Manufacturer/Model: GE PG7221 FA
 Fuel Type: Distillate Oil
 Load: 70%
 Ambient Temperature: 97°F

- Arsenic: 4.2 lb/10¹² Btu x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 5.08x10⁻³ lb/hr
- Beryllium: 2.5 lb/10¹² Btu x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.02x10⁻³ lb/hr
- Mercury: 3.0 lb/10¹² Btu x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.63x10⁻³ lb/hr
- Fluoride: 14.0 pg/J x 2.324 lb/10¹² Btu/pg/J x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 3.94x10⁻² lb/hr
- Nickel: 170 lb/10¹² Btu x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.206 lb/hr
- Cadmium: 10.5 lb/10¹² Btu x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 1.27x10⁻² lb/hr
- Chromium: 47.5 lb/10¹² Btu x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 5.75x10⁻² lb/hr
- Copper: 280 lb/10¹² Btu x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.339 lb/hr
- Vanadium: 69.5 lb/10¹² Btu x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 8.41x10⁻² lb/hr
- Selenium: 23.42 lb/10¹² Btu x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 2.83x10⁻² lb/hr
- Polycyclic Organic Matter: 0.278 lb/10¹² Btu x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 3.36x10⁻⁴ lb/hr
- Formaldehyde: 405 lb/10¹² Btu x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.490 lb/hr
- Antimony: 9.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 2.64x10⁻² lb/hr
- Barium: 8.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 2.36x10⁻² lb/hr
- Cobalt: 3.9 pg/J x 2.324 lb/10¹² Btu/pg/J x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 1.10x10⁻² lb/hr
- Zinc: 294 pg/J x 2.324 lb/10¹² Btu/pg/J x 1209.6 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 0.826 lb/hr
- Chlorine: 0.5 ppm x 65206.5 lb/hr fuel oil + 10⁶ - 3.26x10⁻² lb/hr

GE PG7221 FA
 NATURAL GAS
 70% LOAD
 27°F

12018G2/APPA-1
 06/15/92
 7/30/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - 27°F CONDITIONS

(From Table A-2 On ~~Distillate Oil~~; ^{6A} NATURAL GAS; 70% LOAD)

All Other Calculations on Spreadsheet are Identical.)

^{6A}
 Table A-2: (Note: all other data not calculated but supplied by
 Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 119,900 \quad 10,770 \quad 1,291.3 \\ 1,837,000 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas

~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,291.3 \quad 21,515 \quad 60,019.7 \\ 1,849.9 \times 10^6 + 18,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,744,000 \quad 1,177 \quad 28.45 \\ 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 1,920,685 \\ - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68^\circ\text{F} \\ 2,744,000 \quad 28.45 \\ 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 619,500 \\ - 851,152 \text{ scfm} \end{array}$$

GE PG7221 FA
 Natural Gas
 70% LOAD
 27°F

12018C2/APPA-2
 06/13/92
 7/30/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{1,920,685}{2,450,287} \text{ acfm} \times \frac{200}{(205^\circ\text{F} + 460^\circ\text{F})} + \frac{1,177}{(1,060^\circ\text{F} + 460^\circ\text{F})}$$

$$= \frac{774,375}{1,072,001} \text{ acfm}$$

Velocity (ft/sec):

$$\frac{\text{Volume Flow (ft}^3\text{/min)} + \text{Area (ft}^2\text{)} + 60 \text{ sec/min}}{1,072,001 \text{ ft}^3\text{/min} + 60 + (18.0^2 + 4 \times 3.14159)}$$

$$= \frac{774,375}{50.7} = 70.2 \text{ ft/sec}$$

7A
 Table A-2:

PM emissions in tons per year

$$\frac{9.0}{17} \text{ lb/hr} \times 8460 \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$= \frac{38.07}{2.6} \text{ ton/yr}$$

GAS
 SO₂ Emissions - ~~oil~~ (lb/hr)

$$\frac{1,359,287 \text{ cf/hr}}{69,722.9 \text{ lb/hr}} \times \frac{1.0 \text{ gr/100 cf}}{0.0005 \text{ lb S/lb}} \times 2 \text{ lb SO}_2\text{/lb S} \times 1.0 \text{ lb/7000 gr}$$

$$= \frac{3.88}{99.72} \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$\frac{25}{42} \text{ ppm} \times \left[\frac{7.84}{20.9} \times \left(1 - \frac{11.59}{100} \right) - \frac{12.46}{10.96} \right] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{1,920,685}{2,450,287} \text{ ft}^3\text{/min}$$

$$\times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + \left[\frac{1,545}{3.64} \times \frac{1,177}{(1,060^\circ\text{F} + 460^\circ\text{F})} \right]$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$= \frac{127.9}{326.2} \text{ lb/hr}$$

GE PG7221 FA
 Natural Gas
 70% Load
 27°F

12018C2/APPA-3
 06/12/92
 7/30/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 15 \quad 7.84 \quad 1,920,685 \\
 & 30 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,177} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,060}{1,177} \text{ F} + 460 \text{ F}) \times 10^6) \\
 & \quad 373 \\
 & - 98.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 1.5 \quad 7.84 \quad 1,920,685 \\
 & 3.5 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,177} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,060}{1,177} \text{ F} + 460 \text{ F}) \times 10^6) \\
 & \quad 2.13 \\
 & - 6.56 \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\frac{8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr}}{1.65 \times 10^{-2} \text{ lb/hr}}$$

8A

Table A-5:

H₂SO₄ Mist Emissions (lb/hr):

$$\begin{aligned}
 & \text{Based on 8 percent of sulfur converted to acid mist} \\
 & \left(\frac{1,359,287 \text{ cf/hr}}{99,722.9 \text{ lb/hr}} \times \frac{1.09 \text{ cf}}{100 \text{ cf}} \times \frac{216 \text{ SO}_2}{16 \text{ S}} \times \frac{1.0 \text{ lb}}{7000 \text{ gr}} \right) \times 0.08 \\
 & \quad \text{(converted)} \quad 1.53 \quad 0.05 \\
 & \quad 0.476 \\
 & - 12.2 \text{ lb/hr}
 \end{aligned}$$

A-8A, A-9A, A-10A

Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \frac{1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu}}{2.50 \times 10^{-2} \text{ lb/hr}} \quad \text{Not Applicable}
 \end{aligned}$$

7/30/92

Emission Calculations, Tables A-8A, A-9A, A-10A

Manufacturer/Model: GE PG7221 FA
 Fuel Type: Natural Gas
 Load: 70%
 Ambient Temperature: 27°F

Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1291.3 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 1.44 × 10⁻³ lb/hr

Formaldehyde: 88.12 lb/10¹² Btu x 1291.3 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.114 lb/hr

Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ - NA lb/hr

GE PG 7221 FA
 NATURAL GAS
 70% LOAD
 64°F

12018G2/APPA-1
 06/13/92
 7/30/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁶⁴27°F CONDITIONS

(From Table A-~~2~~^{6A} On ~~Distillate Oil~~; ^{Natural Gas} 70% LOAD)

All Other Calculations on Spreadsheet are Identical.)

^{6A} Table A-~~2~~^{6A}: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 106,500 \quad 11,070 \quad 1,179.0 \\ \hline 1,849,700 \times 10,070/10^6 = 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas

~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,179.0 \quad 21,515 \quad 54,796.9 \\ \hline 1,849.9 \times 10^6 + 18,550 = 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,595,000 \quad 1,195 \quad 28.32 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ \text{F} + 460^\circ \text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ \hline 1,845,077 \\ - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68^\circ \text{F} \\ 2,595,000 \quad 28.32 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ \text{F} + 460^\circ \text{F}) + (28.25 \times 2,116.8) + 60 \\ \hline 588,641 \\ = 851,132 \text{ scfm} \end{array}$$

GE PG7221 FA
 NATURAL GAS
 70% LOAD
 61°F

12018C2/APPA-:
 06/13/91
 7/30/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{1,845,077}{2,450,287} \text{ acfm} \times \frac{200}{(200^\circ\text{F} + 460^\circ\text{F})} + \frac{1,195}{(1,060^\circ\text{F} + 460^\circ\text{F})}$$

$$735,801$$

$$- 1,072,001 \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\frac{735,801}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$18.2$$

$$- 70.2 \text{ ft/sec}$$

A-7A
 Table A-2:

PM emissions in tons per year

$$\frac{9.0}{17} \text{ lb/hr} \times \frac{8460}{300} \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$38.07$$

$$- 2.6 \text{ ton/yr}$$

GAS
 SO₂ Emissions - ~~0.1~~ (lb/hr)

$$\frac{1,241,005 \text{ cf/hr}}{99,722.9} \times \frac{1.09 \text{ lb}}{100 \text{ cf}} \times 2 \text{ lb SO}_2/\text{lb S} \times \frac{1 \text{ lb}}{7000 \text{ gr}}$$

$$3.55$$

$$- 99.72 \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$\frac{25}{42} \text{ ppm} \times \left[20.9 \times \left(1 - \frac{8.98}{11.59} / 100 \right) - 10.96 \right] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{2,450,287}{1,845,077} \text{ ft}^3/\text{min}$$

$$\times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + \left[1,545 \times \frac{1,195}{(1,060^\circ\text{F} + 460^\circ\text{F})} \right]$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$118.1$$

$$- 326.2 \text{ lb/hr}$$

GE PG7221 FA
 Natural Gas
 70% Load
 64°F

12018C2/APPA-3
 06/12/92
 7/30/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned} & 15 \text{ ppm} \times (1 - \frac{8.98}{11.59/100}) \times \frac{1,845,077}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\ & \text{(molecular wgt. of carbon)} \\ & \times 60 \text{ min/hr} + (1,545 \times \frac{1,195}{1,060^\circ\text{F} + 460^\circ\text{F}}) \times 10^6 \\ & 35.0 \\ & - 98.4 \text{ lb/hr} \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned} & 1.5 \text{ ppm} \times (1 - \frac{8.98}{11.59/100}) \times \frac{1,845,077}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\ & \text{(molecular wgt. of methane)} \\ & \times 60 \text{ min/hr} + (1,545 \times \frac{1,195}{1,060^\circ\text{F} + 460^\circ\text{F}}) \times 10^6 \\ & 2.00 \\ & - 6.56 \text{ lb/hr} \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\cancel{8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr} = 1.65 \times 10^{-2} \text{ lb/hr}}$$

A-8A
 Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

$$\begin{aligned} & \text{Based on 8 percent of sulfur converted to acid mist} \\ & \underbrace{1,241,005 \text{ cf/hr} \times 1.09 \text{ lb}/100 \text{ cf} \times 216 \text{ SO}_2 / 16.5 \times 1.0 \text{ lb}/7000 \text{ gr}}_{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4 / \text{lb SO}_2 \times 0.05} \\ & \text{(converted)} \quad 1.53 \\ & 0.434 \\ & - 12.2 \text{ lb/hr} \end{aligned}$$

A-8A, A-9A, A-10A
 Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned} & \cancel{1,849.9 \text{ (MMBtu)} \times 1/4 \text{ lb}/10^{12} \text{ Btu}} \text{ *Not Applicable*} \\ & \cancel{2.59 \times 10^{-2} \text{ lb/hr}} \end{aligned}$$

7/30/92

Emission Calculations, Tables A-8A, A-9A, A-10A

Manufacturer/Model: GE PG7221 FA
 Fuel Type: NATURAL GAS
 Load: 70%
 Ambient Temperature: 64°F

Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1179.0 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - 1.31 × 10⁻³ lb/hr

Formaldehyde: 88.12 lb/10¹² Btu x 1179.0 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.104 lb/hr

Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 - NA lb/hr

Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ - NA lb/hr

GE PG7221FA
 NATURAL GAS
 70% LOAD
 72°F

12018C2/APPA-1
 06/13/92
 7/30/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁷²°F CONDITIONS

(From Table A-7 On ^{6A} ~~Distillate Oil~~; ^{NATURAL GAS} 70% LOAD)

All Other Calculations on Spreadsheet are Identical.)

^{6A}
 Table A-7: (Note: all other data not calculated but supplied by
 Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 103,100 \quad 11,340 \quad 1169.2 \\ \hline 1,837,700 \times 16,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas

~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1169.2 \quad 21,515 \quad 54,341.3 \\ \hline 1,849.9 \times 10^6 + 18,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,560,000 \quad 1,199 \quad 28.27 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,066^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 1,827,352 \\ - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

$$\begin{array}{r} \text{Same as volume flow (acfm) except adjusted for standard temperature of} \\ 68^\circ\text{F} \\ 2,560,000 \quad 28.27 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 581,580 \\ - 851,152 \text{ scfm} \end{array}$$

GE PG7221FA
 Natural Gas
 70% Load
 72°F

12018C2/APPA-2
 06/13/92
 7/30/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{1,827,352}{2,450,287} \text{ acfm} \times \frac{200}{(205^\circ\text{F} + 460^\circ\text{F}) + \frac{1,199}{(1,060^\circ\text{F} + 460^\circ\text{F})}}$$

$$= \frac{726,975}{1,072,001} \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\frac{726,975}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$= \frac{47.6}{70.2} \text{ ft/sec}$$

7A
 Table A-2:

PM emissions in tons per year

$$\frac{9.0}{17} \text{ lb/hr} \times \frac{8460}{300} \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$= \frac{38.07}{2.6} \text{ ton/yr}$$

GAS
 SO₂ Emissions - Oil (lb/hr)

$$\frac{1,230,688 \text{ cf/hr}}{99,722.9} \text{ lb/hr} \times \frac{1.09 \text{ gr/100 cf}}{0.0005 \text{ lb S/lb}} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.016/7000 \text{ gr}$$

$$= \frac{3.52}{99.72} \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$\frac{25}{42} \text{ ppm} \times \left[20.9 \times \left(1 - \frac{9.34}{100} \right) - \frac{12.39}{10.96} \right] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{1,827,352}{2,450,287} \text{ ft}^3/\text{min}$$

$$\times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + \left[1,545 \times \frac{1,199}{(1,060^\circ\text{F} + 460^\circ\text{F})} \right]$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$= \frac{115.7}{326.2} \text{ lb/hr}$$

GE P07221 FA
 Natural Gas
 70% Load
 72°F

12018C2/APPA-3
 06/12/92
 7/30/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 15 \quad 9.34 \quad 1,827,352 \\
 & 30 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{2,116.8} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,199}{1,960} \times (72^\circ\text{F} + 460^\circ\text{F}) \times 10^6) \\
 & \quad 34.5 \\
 & - 98.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 1.5 \quad 9.34 \quad 1,827,352 \\
 & 2.5 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{2,116.8} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,199}{1,960} \times (72^\circ\text{F} + 460^\circ\text{F}) \times 10^6) \\
 & \quad 2.00 \\
 & - 6.56 \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\frac{8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr}}{1.65 \times 10^{-2}} \text{ lb/hr}$$

8A
 Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

$$\begin{aligned}
 & \text{Based on 8 percent of sulfur converted to acid mist} \\
 & \frac{1,230,688 \text{ cf/hr} \times 1.09 \text{ lb SO}_2 / 100 \text{ cf} \times 2 \text{ lb SO}_2 / 165 \times 1.016 / 7000 \text{ gr}}{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4 / \text{lb SO}_2 \times 0.05} \\
 & \quad \text{(converted)} \quad 1.53 \quad 0.08 \\
 & \quad 0.431 \\
 & - 12.2 \text{ lb/hr}
 \end{aligned}$$

A-8A, A-9A, A-10A
 Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \frac{1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu}}{2.59 \times 10^{-2}} \text{ lb/hr} \quad \text{Not Applicable} \\
 & - 2.59 \times 10^{-2} \text{ lb/hr}
 \end{aligned}$$

7/30/92

Emission Calculations, Tables A-8A, A-9A, A-10A

Manufacturer/Model: GE PG7221FA

Fuel Type: Natural Gas

Load: 70%

Ambient Temperature: 72°F

Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1169.2 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= 1.3 × 10⁻³ lb/hr

Formaldehyde: 88.12 lb/10¹² Btu x 1169.2 MMBtu/hr + 10⁶ MMBtu/10¹² Btu = 0.103 lb/hr

Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ = NA lb/hr

GE PG7221 FA
 NATURAL GAS
 70% LOAD
 79°F

12018C2/APPA-1
 06/13/92
 7/30/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁷⁹°F CONDITIONS

(From Table A-^{6A} On ~~Distillate Oil~~; ^{NATURAL GAS} 70% LOAD)

All Other Calculations on Spreadsheet are Identical.)

^{6A}
 Table A-~~1~~: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 99,500 \quad 11,510 \quad 1,145.2 \\ \hline 1,145,200 \times 10^6 / 10^6 - 1,145.2 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas

~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,145.2 \quad 21,515 \quad 53,230.1 \\ \hline 1,145.2 \times 10^6 + 10,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,524,000 \quad 1,200 \quad 28.18 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 1,808,470 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68^\circ\text{F} \\ 2,524,000 \quad 28.18 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 575,224 \\ \hline - 851,152 \text{ scfm} \end{array}$$

GE PG7221 FA
 NATURAL GAS
 70% LOAD
 79°F

12018C2/APPA-2
 06/15/92
 7/30/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{1,808,470}{2,450,287} \text{ acfm} \times \frac{200}{(205^\circ\text{F} + 460^\circ\text{F})} + \frac{1,200}{(1,060^\circ\text{F} + 460^\circ\text{F})}$$

$$= \frac{719,030}{1,072,001} \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) ÷ Area (ft²) ÷ 60 sec/min

$$\frac{719,030}{1,072,001} \text{ ft}^3/\text{min} \div 60 \div (18.0^2 + 4 \times 3.14159)$$

$$= \frac{47.1}{70.2} \text{ ft/sec}$$

7A
 Table A-8:

PM emissions in tons per year

9.0 8460

$$\frac{17 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton}}{38.07}$$

$$= 2.6 \text{ ton/yr}$$

GAS
 SO₂ Emissions - 0.1 (lb/hr)

$$\frac{1,205,521 \text{ cf/hr}}{99,722.9 \text{ lb/hr}} \times \frac{1.0 \text{ gr}}{100 \text{ cf}} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb}/7000 \text{ gr}$$

$$= \frac{3.44}{99.72} \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

25 10.14 12.28

$$\frac{42 \text{ ppm} \times [20.9 \times (1 - \frac{11.59}{100}) - 10.96]}{1,808,470} \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{1,200}{(1,060^\circ\text{F} + 460^\circ\text{F})}$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$= \frac{113.5}{326.2} \text{ lb/hr}$$

GE PG7221 FA
 Natural Gas
 70% LOAD
 79°F

12018C2/APPA-3
 06/12/92
 7/30/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 15 \quad 10.14 \quad 1,808,470 \\
 & 30 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,200} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,200}{1,060} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad 338 \\
 & - 98.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 1.6 \quad 10.14 \quad 1,808,470 \\
 & 3.5 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,200} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,200}{1,060} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad 2.06 \\
 & - 6.56 \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\frac{8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr}}{1.65 \times 10^{-2} \text{ lb/hr}}$$

A-8A

Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned}
 & \frac{1,205,521 \text{ cf/hr} \times 1.0 \text{ gr}/100 \text{ cf} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb}/7000 \text{ gr}}{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S}/\text{lb} \times 3.86 \text{ lb H}_2\text{SO}_4/\text{lb SO}_2 \times 0.05} \\
 & \quad \text{(converted)} \quad 1.53 \\
 & \quad 0.422 \\
 & - 12.2 \text{ lb/hr}
 \end{aligned}$$

A-8A, A-9A, A-10A

Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \frac{1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu}}{2.59 \times 10^{-2} \text{ lb/hr}} \quad \text{NOT Applicable} \\
 & = 2.59 \times 10^{-2} \text{ lb/hr}
 \end{aligned}$$

7/30/92

Emission Calculations, Tables A-8A, A-9A, A-10A

Manufacturer/Model: PG 7221 FA
 Fuel Type: Natural Gas
 Load: 70%
 Ambient Temperature: 79°F

Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1145.2 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = 1.27 × 10⁻³ lb/hr

Formaldehyde: 88.12 lb/10¹² Btu x 1145.2 MMBtu/hr + 10⁶ MMBtu/10¹² Btu = 0.101 lb/hr

Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ = NA lb/hr

GE PG 7221 FA
 NATURAL GAS
 70% LOAD
 97°F

12018C2/APPA-1
 06/13/92
 7/30/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁹⁷°F CONDITIONS

(From Table A-1 On ~~Distillate Oil~~; ^{6A} NATURAL GAS; 70% LOAD)

All Other Calculations on Spreadsheet are Identical.)

^{6A}
 Table A-1: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 90,900 \quad 11,890 \quad 1,080.8 \\ \hline 1,073,700 \times 10^6 / 10^6 = 1,073,700 \times 10^6 \text{ Btu/hr} \end{array}$$

NATURAL GAS

~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,080.8 \quad 21,515 \quad 50,234.8 \\ \hline 1,080.8 \times 10^6 + 10,550 = 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,454,000 \quad 1,200 \quad 28.20 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ \hline 1,757,157 \\ - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

$$\begin{array}{r} \text{Same as volume flow (acfm) except adjusted for standard temperature of} \\ 68^\circ\text{F} \\ 2,454,000 \quad 28.20 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ \hline 558,903 \\ - 851,152 \text{ scfm} \end{array}$$

GE PG7221 FA
 Natural Gas
 70% LOAD
 97°F

12018C2/APPA-2
 06/13/92
 7/30/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{1,757,157}{2,450,287} \text{ acfm} \times \frac{200}{(205^\circ\text{F} + 460^\circ\text{F})} + \frac{1,200}{(1,060^\circ\text{F} + 460^\circ\text{F})}$$

$$= \frac{698,629}{1,072,001} \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) ÷ Area (ft²) ÷ 60 sec/min

$$\frac{698,629}{1,072,001} \text{ ft}^3/\text{min} \div 60 \div (18.0^2 + 4 \times 3.14159)$$

$$= \frac{45.8}{70.2} \text{ ft/sec}$$

7A
 Table A-2:

PM emissions in tons per year

$$\frac{9.0}{17} \text{ lb/hr} \times \frac{8460}{300} \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$= \frac{38.07}{2.6} \text{ ton/yr}$$

GAS
 SO₂ Emissions - oil (lb/hr)

$$\frac{1,137,685 \text{ cf/hr}}{99,722.9} \text{ lb/hr} \times \frac{1.0 \text{ gr}}{100 \text{ cf}} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb}/7000 \text{ gr}$$

$$= \frac{3.25}{99.72} \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$\frac{25}{42} \text{ ppm} \times [20.9 \times (1 - \frac{9.89}{11.59/100}) - \frac{12.52}{10.96}] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{1,757,157}{2,450,287} \text{ ft}^3/\text{min}$$

$$\times 46 \text{ (molecular wgt NO}_2) \times 60 \text{ min/hr} + [1,545 \times \frac{1,200}{(1,060^\circ\text{F} + 460^\circ\text{F})}]$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$= \frac{107.1}{326.2} \text{ lb/hr}$$

GE PG7221 FA
 NATURAL GAS
 70% LOAD
 97°F

12018C2/APPA-3
 06/12/92
 7/30/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 15 \text{ ppm} \times (1 - \frac{9.89}{11.59}/100) \times \frac{1,757,157}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,200}{1,060} \text{°F} + 460 \text{°F}) \times 10^6 \\
 & \quad - 32.9 \\
 & \quad - 98.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 1.5 \text{ ppm} \times (1 - \frac{9.89}{11.59}/100) \times \frac{1,757,157}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,200}{1,060} \text{°F} + 460 \text{°F}) \times 10^6 \\
 & \quad - 1.88 \\
 & \quad - 6.56 \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\frac{8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr}}{1.65 \times 10^{-2} \text{ lb/hr}}$$

^{8A}
 Table A-2:

H₂SO₄ Mist Emissions (lb/hr):

$$\begin{aligned}
 & \text{Based on 8 percent of sulfur converted to acid mist} \\
 & \frac{1,137,685 \text{ cf/hr} \times 1.0 \text{ gr}/100 \text{ cf} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb}/7000 \text{ gr}}{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb SO}_2 \times 0.05} \\
 & \quad \text{(converted)} \quad \quad \quad 1.53 \\
 & \quad \quad \quad 0.398 \\
 & \quad - 12.2 \text{ lb/hr}
 \end{aligned}$$

A-8A, A-9A, A-10A
 Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \frac{1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu}}{2.59 \times 10^{-2} \text{ lb/hr}} \quad \text{Not Applicable}
 \end{aligned}$$

7/30/92

Emission Calculations, Tables A-8A, A-9A, A-10A

Manufacturer/Model: GE PG7221 FA
Fuel Type: NATURAL GAS
Load: 70%
Ambient Temperature: 97°F

- Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr
- Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr
- Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr
- Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr
- Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr
- Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr
- Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr
- Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr
- Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr
- Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr
- Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1080.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= 1.2x10⁻³ lb/hr
- Formaldehyde: 88.12 lb/10¹² Btu x 1080.8 MMBtu/hr + 10⁶ MMBtu/10¹² Btu = 9.52x10⁻² lb/hr
- Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr
- Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr
- Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr
- Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr
- Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ = NA lb/hr

WEST 501 F
 DISTILLATE OIL
 BASE LOAD
 27°F

12018C2/APPA-1
 06/13/92
 8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - 27°F CONDITIONS

(From Table A-¹⁹ On Distillate Oil; BASE LOAD

All Other Calculations on Spreadsheet are Identical.)

¹⁹
Table A-1: (Note: all other data not calculated but supplied by
 Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 171,970 \quad 9,280 \quad 1,595.9 \\ \hline 183,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Fuel Oil (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,595.9 \quad 18,450 \quad 86,498 \\ \hline 1,849.9 \times 10^6 + 18,550 = 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 3,502,180 \quad 1,104 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25^{33} \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,351,909 \\ \hline = 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68^\circ\text{F} \\ 3,502,180 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25^{33} \times 2,116.8) + 60 \\ 793,995 \\ \hline = 851,152 \text{ scfm} \end{array}$$

WEST 501 F
DISTILLATE OIL
BASE LOAD
27 °F

12018C2/APPA-2
06/13/92
8/26/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature
$$\begin{aligned} & 2,351,909 \\ & \frac{2,450,287 \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + (1,060^\circ\text{F} + 460^\circ\text{F})}{1,000,012} \\ & - 1,072,001 \text{ acfm} \end{aligned}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min
$$\begin{aligned} & \frac{1,000,012}{1,072,001 \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)} \\ & 65.5 \\ & - 70.2 \text{ ft/sec} \end{aligned}$$

²⁰
Table A-2:

PM emissions in tons per year
$$\begin{aligned} & 39.5 \\ & \frac{17 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton}}{5.9} \\ & - 2.6 \text{ ton/yr} \end{aligned}$$

SO₂ Emissions--Oil (lb/hr)

$$\begin{aligned} & 66,497.6 \\ & \frac{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2/\text{lb S}}{87.35} \\ & - 99.72 \text{ lb/hr} \end{aligned}$$

NO_x Emissions (lb/hr) - See Note B:

$$\begin{aligned} & 44.5 \\ & \frac{42 \text{ ppm} \times [20.9 \times (1 - \frac{10.6}{100}) - 10.96] \times 2,116.8 \text{ lb/ft}^2}{2,351,909} \\ & \times 2,450,287 \text{ ft}^3/\text{min} \\ & \times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times \frac{1,104}{(1,060^\circ\text{F} + 460^\circ\text{F})}] \\ & \times 5.9 \times 10^6 \text{ (adjust for ppm)} \\ & - 326.2 \text{ lb/hr} \\ & 290.1 \end{aligned}$$

WEST 501 F
 DISTILLATE OIL
 BASE LOAD
 27 °F

12018C2/APPA-3
 06/12/92
 8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & \frac{52}{30} \text{ ppm} \times \left(1 - \frac{10.6}{11.59}\right) \times \frac{2,351,909}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,104}{1,060} \times 10^6) \\
 & \quad - \frac{160.9}{98.4} \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & \frac{10.6}{3.5} \text{ ppm} \times \left(1 - \frac{10.6}{11.59}\right) \times \frac{2,351,909}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,104}{1,060} \times 10^6) \\
 & \quad - \frac{18.7}{6.56} \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr):

$$8.9 \text{ lb}/10^{12} \text{ Btu} \times \frac{1,595.9}{1,849.9} \times 10^6 \text{ Btu/hr} - \frac{1.42}{1.65} \times 10^{-2} \text{ lb/hr}$$

Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

$$\begin{aligned}
 & \text{Based on 8 percent of sulfur converted to acid mist} \\
 & \frac{86,498}{99,722.9} \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb S} \times \frac{0.08}{0.05} \\
 & \quad \text{(converted)} \\
 & \quad - \frac{10.9}{12.2} \text{ lb/hr}
 \end{aligned}$$

²²
Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \frac{1,595.9}{1,849.9} \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu} \\
 & \quad - \frac{2.32}{2.59} \times 10^{-2} \text{ lb/hr}
 \end{aligned}$$

8/26/92
7/31/92

Emission Calculations, Tables A-21, A-22, A-23

Manufacturer/Model: West 501F
Fuel Type: Distillate Oil
Load: Base
Ambient Temperature: 27°F

- Arsenic: 4.2 lb/10¹² Btu x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 6.7 × 10⁻³ lb/hr
- Beryllium: 2.5 lb/10¹² Btu x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.99 × 10⁻³ lb/hr
- Mercury: 3.0 lb/10¹² Btu x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 4.79 × 10⁻³ lb/hr
- Fluoride: 14.0 pg/J x 2.324 lb/10¹² Btu/pg/J x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- 5.19 × 10⁻² lb/hr
- Nickel: 170 lb/10¹² Btu x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 2.71 × 10⁻² lb/hr
- Cadmium: 10.5 lb/10¹² Btu x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 1.68 × 10⁻² lb/hr
- Chromium: 47.5 lb/10¹² Btu x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 7.58 × 10⁻² lb/hr
- Copper: 280 lb/10¹² Btu x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.447 lb/hr
- Vanadium: 69.5 lb/10¹² Btu x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.111 lb/hr
- Selenium: 23.42 lb/10¹² Btu x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.74 × 10⁻² lb/hr
- Polycyclic Organic Matter: 0.278 lb/10¹² Btu x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- 4.44 × 10⁻⁴ lb/hr
- Formaldehyde: 405 lb/10¹² Btu x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.646 lb/hr
- Antimony: 9.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- 3.49 × 10⁻² lb/hr
- Barium: 9.4 pg/J x 2.324 lb/10¹² Btu/pg/J x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- 3.11 × 10⁻² lb/hr
- Cobalt: 3.9 pg/J x 2.324 lb/10¹² Btu/pg/J x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- 1.45 × 10⁻² lb/hr
- Zinc: 294 pg/J x 2.324 lb/10¹² Btu/pg/J x 1595.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- 1.09 lb/hr
- Chlorine: 0.5 ppm x 88142.1 lb/hr fuel oil + 10⁶ - 4.41 × 10⁻² lb/hr

WEST 501 F
DISTILLATE OIL
BASE LOAD
72°F

12018C2/APPA-1
06/13/92
8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁷²27°F CONDITIONS

(From Table A-¹⁹1 On Distillate Oil; BASE LOAD)

All Other Calculations on Spreadsheet are Identical.)

¹⁹Table A-1: (Note: all other data not calculated but supplied by
Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 162,330 \quad 9,560 \quad 1,551.9 \\ \hline 183,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Fuel Oil (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,551.9 \quad 18,450 \quad 84,112.5 \\ \hline 1,849.9 \times 10^6 + 18,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 3,509,380 \quad 1,104 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25^{17} \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,370,209 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

$$\begin{array}{r} \text{Same as volume flow (acfm) except adjusted for standard temperature of} \\ 68^\circ\text{F} \\ 3,509,380 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25^{17} \times 2,116.8) + 60 \\ 800,173 \\ \hline - 851,152 \text{ scfm} \end{array}$$

WEST 501 F
 DISTILLATE OIL
 BASE LOAD
 72 °F

12018C2/APPA-2
~~06/13/92~~
 8/26/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$2,379,209$$

$$2,450,287 \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + \overset{1,104}{(-1,060^\circ\text{F} + 460^\circ\text{F})}$$

$$1,007,794$$

$$- 1,072,001 \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$1,007,794$$

$$1,072,001 \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$66.0$$

$$= 70.2 \text{ ft/sec}$$

²⁰
 Table A-2:

PM emissions in tons per year

$$39$$

$$17 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$5.9$$

$$= 2.6 \text{ ton/yr}$$

SO₂ Emissions--Oil (lb/hr)

$$64,112.5$$

$$99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2/\text{lb S}$$

$$86.22$$

$$= 99.72 \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$42.7$$

$$42 \text{ ppm} \times [20.9 \times (1 - \overset{91}{11.59}/100) - \overset{11.88}{10.96}] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{2,450,287 \text{ ft}^3/\text{min}}{2,379,209}$$

$$\times 46 \text{ (molecular wgt NO}_2) \times 60 \text{ min/hr} + [1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F})$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}]$$

$$270.9$$

$$= 326.2 \text{ lb/hr}$$

WEST 501 F
DISTILLATE OIL
BASE LOAD
72°F

12018C2/APPA-3
06/12/92
8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned} & 51.6 \quad 91 \quad 2,370,290 \\ & 30 \text{ ppm} \times (1 - 11.59/100) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\ & \quad \text{(molecular wgt. of carbon)} \\ & \times 60 \text{ min/hr} + (1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) \times 10^6) \\ & \quad 158.4 \\ & - 98.4 \text{ lb/hr} \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned} & 10.5 \quad 91 \quad 2,370,209 \\ & 3.5 \text{ ppm} \times (1 - 11.59/100) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\ & \quad \text{(molecular wgt. of methane)} \\ & \times 60 \text{ min/hr} + (1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) \times 10^6) \\ & \quad 18.44 \\ & - 6.56 \text{ lb/hr} \end{aligned}$$

Lead Emissions (lb/hr):

$$8.9 \text{ lb}/10^{12} \text{ Btu} \times \frac{1,551.9}{1,849.9} \times 10^6 \text{ Btu/hr} - 1.65 \times 10^{-2} \text{ lb/hr} \quad 38$$

²¹
Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned} & 84,112.5 \quad 8 \\ & 99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb S} \times 0.08 \\ & \quad \text{(converted)} \\ & \quad 10.6 \\ & - 12.2 \text{ lb/hr} \end{aligned}$$

²²
Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned} & 1,551.9 \\ & 1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu} \\ & \quad 2.17 \\ & - 2.59 \times 10^{-2} \text{ lb/hr} \end{aligned}$$

7/31/92
8/26/92

Emission Calculations, Tables A-21, A-22, A-23

Manufacturer/Model: West. 501F
Fuel Type: Distillate Oil
Load: BASE
Ambient Temperature: 72°F

- Arsenic: 4.2 lb/10¹² Btu x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{6.52}~~6.45~~ × 10⁻³ lb/hr
- Beryllium: 2.5 lb/10¹² Btu x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.88 × 10⁻³ lb/hr
- Mercury: 3.0 lb/10¹² Btu x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 4.61 × 10⁻³ lb/hr
- Fluoride: 14.0 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- 5.0 × 10⁻² lb/hr
- Nickel: 170 lb/10¹² Btu x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.264 lb/hr
- Cadmium: 10.5 lb/10¹² Btu x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{1.63}~~1.63~~ × 10⁻² lb/hr
- Chromium: 47.5 lb/10¹² Btu x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{7.37}~~7.37~~ × 10⁻² lb/hr
- Copper: 280 lb/10¹² Btu x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.435 lb/hr
- Vanadium: 69.5 lb/10¹² Btu x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.108 lb/hr
- Selenium: 23.42 lb/10¹² Btu x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{3.63}~~3.63~~ × 10⁻² lb/hr
- Polycyclic Organic Matter: 0.278 lb/10¹² Btu x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- 4.27 × 10⁻⁴ lb/hr
- Formaldehyde: 405 lb/10¹² Btu x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu 0.622 lb/hr
- Antimony: 9.4 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- 3.38 × 10⁻² lb/hr
- Barium: 8.4 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- ^{3.03}~~3.03~~ × 10⁻² lb/hr
- Cobalt: 3.9 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- ^{1.41}~~1.41~~ × 10⁻² lb/hr
- Zinc: 294 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{51.9}~~15385~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- 1.06 lb/hr
- Chlorine: 0.5 ppm x 84,887.5 lb/hr fuel oil + 10⁶ - ^{4.21}~~4.21~~ × 10⁻² lb/hr

WEST 501 F
 DISTILLATE OIL
 BASE LOAD
 97 °F

12018C2/APPA-1
 06/13/92
 8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁹⁷27 °F CONDITIONS

(From Table A-1¹⁹ On Distillate Oil; BASE LOAD

All Other Calculations on Spreadsheet are Identical.)

¹⁹
 Table A-1: (Note: all other data not calculated but supplied by
 Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW) x Heat Rate (10}^6 \text{ Btu/kWh)} \\ 147,180 \quad 9,850 \quad 1,449.7 \\ \hline 1,449.7 \times 10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Fuel Oil (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr) + Fuel Heat Content (Btu/lb)} \\ 1,449.7 \quad 18,450 \quad 78,576 \\ \hline 1,849.9 \times 10^6 + 18,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 3,311,800 \quad 1,121 \quad 28.09 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,267,804 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

$$\begin{array}{r} \text{Same as volume flow (acfm) except adjusted for standard temperature of} \\ 68^\circ\text{F} \\ 3,311,800 \quad 28.09 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 757,369 \\ \hline - 851,152 \text{ scfm} \end{array}$$

WEST 501 F
DISTILLATE OIL
BASE LOAD
97°F

12018C2/APPA-1
06/13/92
8/26/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature
$$\begin{aligned} & 2,267,804 \\ & \cancel{2,450,287} \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + \overset{1,121}{\cancel{1,060}}^\circ\text{F} + 460^\circ\text{F} \\ & \quad 953,883 \\ & - \cancel{1,072,001} \text{ acfm} \end{aligned}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min
$$\begin{aligned} & 953,883 \\ & \cancel{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159) \\ & \quad 62.5 \\ & - \cancel{70.2} \text{ ft/sec} \end{aligned}$$

²⁰
Table A-7:

PM emissions in tons per year
$$\begin{aligned} & 36.7 \\ & \cancel{17} \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton} \\ & \quad 5.5 \\ & - \cancel{2.6} \text{ ton/yr} \end{aligned}$$

SO₂ Emissions--Oil (lb/hr)

$$\begin{aligned} & 78,576 \\ & \cancel{99,722.9} \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2/\text{lb S} \\ & \quad 81.33 \\ & - \cancel{99.72} \text{ lb/hr} \end{aligned}$$

NO_x Emissions (lb/hr) - See Note B:

$$\begin{aligned} & 42.7 \\ & 42 \text{ ppm} \times [20.9 \times (1 - \overset{12.57}{\cancel{11.59}}/100) - \overset{11.83}{\cancel{10.96}}] \times 2,116.8 \text{ lb/ft}^2 \\ & \quad \times \cancel{2,450,287} \text{ ft}^3/\text{min} \\ & \quad \quad 2,267,804 \\ & \quad \times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times \overset{1,121}{\cancel{1,060}}^\circ\text{F} + 460^\circ\text{F}] \\ & \quad \times 5.9 \times 10^6 \text{ (adjust for ppm)} \\ & \quad - \cancel{326.2} \text{ lb/hr} \\ & \quad 252.9 \end{aligned}$$

WEST 501 F
 DISTILLATE OIL
 BASE LOAD
 97 °F

12018G2/APPA-3
 06/12/92
 8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & \overset{51.5}{30} \text{ ppm} \times \left(1 - \frac{12.57}{11.59/100}\right) \times \overset{2,267,804}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \overset{1,121}{1,060} \text{°F} + 460 \text{°F}) \times 10^6 \\
 & \quad \overset{148.7}{- 98.4} \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & \overset{10.5}{3.5} \text{ ppm} \times \left(1 - \frac{12.57}{11.59/100}\right) \times \overset{2,267,804}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \overset{1,121}{1,060} \text{°F} + 460 \text{°F}) \times 10^6 \\
 & \quad \overset{17.32}{- 6.56} \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr):

$$8.9 \text{ lb}/10^{12} \text{ Btu} \times \overset{1,449.7}{1,849.9} \times 10^6 \text{ Btu/hr} - \overset{1.29}{1.65} \times 10^{-2} \text{ lb/hr}$$

²¹
 Table A-7:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned}
 & \overset{78,576}{99,722.9} \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb S} \times 0.08 \\
 & \quad \text{(converted)} \\
 & \quad \overset{9.96}{- 12.2} \text{ lb/hr}
 \end{aligned}$$

²²
 Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \overset{1,449.7}{1,849.9} \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu} \\
 & \quad \overset{2.03}{- 2.59} \times 10^{-2} \text{ lb/hr}
 \end{aligned}$$

7/31/92
8/26/92

Emission Calculations, Tables A-21, A-22, A-23

Manufacturer/Model: West. 501F
Fuel Type: Distillate Oil
Load: Base
Ambient Temperature: 97°F

- Arsenic: 4.2 lb/10¹² Btu x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu ^{6.09}~~6.02~~ × 10⁻³ lb/hr
- Beryllium: 2.5 lb/10¹² Btu x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu ^{3.62}~~3.59~~ × 10⁻³ lb/hr
- Mercury: 3.0 lb/10¹² Btu x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu ^{4.35}~~4.3~~ × 10⁻³ lb/hr
- Fluoride: 14.0 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
^{0.1449.7}
~~4.72~~ × 10⁻² lb/hr
- Nickel: 170 lb/10¹² Btu x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ⁶0.247 lb/hr
- Cadmium: 10.5 lb/10¹² Btu x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ²1.52 × 10⁻² lb/hr
- Chromium: 47.5 lb/10¹² Btu x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ²6.89 × 10⁻² lb/hr
- Copper: 280 lb/10¹² Btu x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ⁶0.402 lb/hr
- Vanadium: 69.5 lb/10¹² Btu x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{1.01 × 10⁻¹}9.27 × 10⁻² lb/hr
- Selenium: 23.42 lb/10¹² Btu x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{3.40}3.36 × 10⁻² lb/hr
- Polycyclic Organic Matter: 0.278 lb/10¹² Btu x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
^{4.03}
~~3.99~~ × 10⁻⁴ lb/hr
- Formaldehyde: 405 lb/10¹² Btu x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.581 lb/hr
- Antimony: 9.4 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
⁷
~~3.13~~ × 10⁻² lb/hr
- Barium: 8.4 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
³
~~2.88~~ × 10⁻² lb/hr
- Cobalt: 3.9 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
⁷
~~1.3~~ × 10⁻² lb/hr
- Zinc: 294 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{49.7}/~~1437.7~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
^{0.991}
~~0.98~~ lb/hr
- Chlorine: 0.5 ppm x ^{78,575.8}/~~78,247.4~~ lb/hr fuel oil + 10⁶ - ³3.98 × 10⁻² lb/hr

WEST. 501F
Natural Gas
Base Load
27°F

12018C2/APPA-1
06/13/92
8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - 27°F CONDITIONS

(From Table A-~~2~~²⁴ On ~~Distillate Oil~~; *Natural Gas*; *Base Load*)

All Other Calculations on Spreadsheet are Identical.)

Table A-~~2~~²⁴: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10^6 Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (} 10^6 \text{ Btu/kWh)} \\ 169,210 \quad 9,490 \quad 1,605.8 \\ \hline 183,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas

~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (} 10^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,605.8 \quad 20,900 \quad 76,832.7 \\ \hline 1,849.9 \times 10^6 + 18,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 3,702,540 \quad 1,063 \quad 28.49 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,407,465 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

$$\begin{array}{r} \text{Same as volume flow (acfm) except adjusted for standard temperature of} \\ 68^\circ\text{F} \\ 3,702,540 \quad 28.49 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 834,630 \\ \hline - 851,152 \text{ scfm} \end{array}$$

WEST. 501F
 Natural Gas
 Base Load
 27°F

12018G2/APPA-2
~~06/13/92~~
 8/26/92

Volume Flow from HRSG (acfm):

$$\begin{aligned}
 & \text{GT Exhaust adjusted for temperature} \\
 & 2,407,465 \\
 & \frac{2,450,287 \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + 1,063}{1,051,191} \\
 & - 1,072,001 \text{ acfm}
 \end{aligned}$$

Velocity (ft/sec):

$$\begin{aligned}
 & \text{Volume Flow (ft}^3\text{/min) + Area (ft}^2\text{) + 60 sec/min} \\
 & \frac{1,051,191}{1,072,001 \text{ ft}^3\text{/min} + 60 + (18.0^2 + 4 \times 3.14159)} \\
 & 68.8 \\
 & - 70.2 \text{ ft/sec}
 \end{aligned}$$

25
 Table A-4:

PM emissions in tons per year

$$\begin{aligned}
 & 6.6 \quad 8460 \\
 & 17 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton} \\
 & 27.92 \\
 & - 2.6 \text{ ton/yr}
 \end{aligned}$$

Nat. Gas

SO₂ Emissions - oil (lb/hr)

$$\begin{aligned}
 & 1690,319 \text{ cf/hr} \quad 19 \text{ lb/100 cf} \\
 & 99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2\text{/lb S} \times 1.0 \text{ lb/7000 gr} \\
 & 4.83 \\
 & - 99.72 \text{ lb/hr}
 \end{aligned}$$

NO_x Emissions (lb/hr) - See Note B:

$$\begin{aligned}
 & 255 \quad 7.26 \quad 13.08 \\
 & 42 \text{ ppm} \times [20.9 \times (1 - \frac{11.59}{100}) - 10.95] \times 2,116.8 \text{ lb/ft}^2 \\
 & \times \frac{2,450,287}{2,407,465} \text{ ft}^3\text{/min} \\
 & \times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times \frac{1,063}{1,060^\circ\text{F} + 460^\circ\text{F}}] \\
 & \times 5.9 \times 10^6 \text{ (adjust for ppm)} \\
 & 162.8 \\
 & - 326.2 \text{ lb/hr}
 \end{aligned}$$

WEST. 501F
 Natural Gas
 Base Load
 27°F

12018C2/APPA-3
 06/12/92
 8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 10.3 \quad 7.26 \quad 2,407,465 \\
 & 90 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{2,407,465} \text{ acfm} \times 2,116.8 \text{ lb/ft}^3 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,063}{1,060} \times (1,060^\circ\text{F} + 460^\circ\text{F}) \times 10^6) \\
 & \quad 34.8 \\
 & - 90.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 4.2 \quad 7.26 \quad 2,407,465 \\
 & 9.9 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{2,407,465} \text{ acfm} \times 2,116.8 \text{ lb/ft}^3 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times \frac{1,063}{1,060} \times (1,060^\circ\text{F} + 460^\circ\text{F}) \times 10^6) \\
 & \quad 8.10 \\
 & - 6.56 \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

~~$8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr} = 1.65 \times 10^{-2} \text{ lb/hr}$~~

²⁶
 Table A-9:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned}
 & \frac{1,690,319 \text{ cf/hr} \times 1.0 \text{ gr}/100 \text{ cf} \times 2.0 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb}/7000 \text{ gr}}{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 1.53 \text{ lb H}_2\text{SO}_4/\text{lb SO}_2} \times 0.08 \\
 & \quad \text{(converted)} \quad 1.53 \quad 0.08 \\
 & \quad 0.623 \\
 & - 12.2 \text{ lb/hr}
 \end{aligned}$$

A-26, A-27, A-28:
 Tables ~~A-4 and A-5~~:

EPA emission factor as noted in printout; example for manganese:

~~$1,849.9 \text{ (lb/Btu)} \times 14 \text{ lb}/10^{12} \text{ Btu} = 2.59 \times 10^{-2} \text{ lb/hr}$~~ *Not Applicable*

Emission Calculations, Tables A-26, A-27, A-28

Manufacturer/Model: West 501F
 Fuel Type: Natural Gas
 Load: Base
 Ambient Temperature: 27°F

Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Polycyclic Organic Matter: 1.113 lb/10¹² Btu x ~~1605.8~~^{1605.8} MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = 1.79 × 10⁻³ lb/hr

Formaldehyde: 88.12 lb/10¹² Btu x ~~1605.8~~^{1605.8} MMBtu/hr + 10⁶ MMBtu/10¹² Btu = 0.140² lb/hr

Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ = NA lb/hr

WEST. 501F
Natural Gas
Base Load
72°F

12018C2/APPA-1
06/13/92
8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁷²72°F CONDITIONS

(From Table A-1 On ²⁴~~Distillate Oil~~; *Natural Gas*; *Base Load*)

All Other Calculations on Spreadsheet are Identical.)

²⁴Table A-1: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10^6 Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (} 10^6 \text{ Btu/kWh)} \\ 1434.50 \quad 10,000 \quad 1,434.5 \\ \hline 1,837,000 \times 10,000 / 10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas

Fuel Oil (lb/hr):

$$\begin{array}{r} \text{Heat Input (} 10^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,434.5 \quad 20,900 \quad 68,636.4 \\ \hline 1,849.9 \times 10^6 + 10,550 - 99,729 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 3,369,010 \quad 1,092 \quad 28.32 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,246,146 \\ \hline - 5,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

$$\begin{array}{r} \text{Same as volume flow (acfm) except adjusted for standard temperature of} \\ 68^\circ\text{F} \\ 3,369,010 \quad 28.32 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 764,153 \\ \hline - 851,152 \text{ scfm} \end{array}$$

WEST. 501F
 NATURAL GAS
 Base LOAD
 72°F

12018G2/APPA-:
 06/23/91
 8/26/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{2,246,146}{2,450,287} \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + \frac{1,092}{1,060} \times (1,060^\circ\text{F} + 460^\circ\text{F})$$

$$= 962,427 - 1,072,001 \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\frac{962,427}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$= 63.0 - 70.2 \text{ ft/sec}$$

25
 Table A-4:

PM emissions in tons per year

$$6.0 \times 8460 \text{ lb/hr} \times 360 \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$= 25.38 - 2.6 \text{ ton/yr}$$

Nat. GAS
 SO₂ Emissions - 0.71 (lb/hr)

$$\frac{1,510,800 \text{ cf/hr}}{99,722.9} \times 1.09 \text{ gr/100 cf} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.016/7000 \text{ gr}$$

$$= 4.31 - 99.72 \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$25.4 \times 42 \text{ ppm} \times \left[20.9 \times \left(1 - \frac{8.82}{11.59} \right) - 10.96 \right] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{2,246,146}{2,450,287} \text{ ft}^3/\text{min}$$

$$\times 46 \text{ (molecular wgt NO}_2) \times 60 \text{ min/hr} + [1,545 \times \frac{1,092}{1,060} \times (1,060^\circ\text{F} + 460^\circ\text{F})]$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$= 144.8 - 126.2 \text{ lb/hr}$$

WEST. 501F
 Natural Gas
 Base LOAD
 72°F

12018C2/APPA-3
 06/12/92
 8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 10.3 \quad 8.82 \quad 2,246,146 \\
 & 30 \text{ ppm} \times (1 - 11.59/100) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^3 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) \times 10^6) \\
 & \quad 1.092 \\
 & \quad 31.3 \\
 & - 98.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 4.1 \quad 8.82 \quad 2,246,146 \\
 & 3.5 \text{ ppm} \times (1 - 11.59/100) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^3 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) \times 10^6) \\
 & \quad 1.092 \\
 & \quad 7.12 \\
 & - 6.56 \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

~~$$8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr} = 1.65 \times 10^{-2} \text{ lb/hr}$$~~

²⁶
 Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned}
 & \underbrace{1,510,000 \text{ cf/hr} \times 1.09 \text{ lb}/100 \text{ cf} \times 2 \text{ lb SO}_2 / \text{lb S} \times 1.0 \text{ lb}/7000 \text{ gr}}_{99,722.9 \text{ lb/hr}} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4 / \text{lb SO}_2 \times 0.05 \\
 & \quad \text{(converted)} \quad 1.53 \\
 & \quad 0.556 \\
 & - 12.2 \text{ lb/hr}
 \end{aligned}$$

A-26, A-27, A-28:

Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

~~$$1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu} = \text{Not Applicable}$$~~

~~$$2.59 \times 10^{-2} \text{ lb/hr}$$~~

Emission Calculations, Tables A-26, A-27, A-28

Manufacturer/Model: West. 501F
 Fuel Type: Natural Gas
 Load: Base
 Ambient Temperature: 72°F

Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1434.5 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
⁶⁰
 = 1.5 × 10⁻³ lb/hr

Formaldehyde: 88.12 lb/10¹² Btu x 1434.5 MMBtu/hr + 10⁶ MMBtu/10¹² Btu = 0.126 lb/hr

Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ = NA lb/hr

West 501F
Natural Gas
Base Load
79°F

12018G2/APPA-1
06/22/92
8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁷⁹27°F CONDITIONS

(From Table A-²⁴3 On ~~Distillate Oil~~; *Natural Gas*; *Base Load*)

All Other Calculations on Spreadsheet are Identical.)

²⁴Table A-3: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10^6 Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (} 10^6 \text{ Btu/kWh)} \\ 139500 \quad 10,100 \quad 1,409.0 \\ \hline 1,409,000 \times 10^6 / 10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas

~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (} 10^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,409.0 \quad 20,900 \quad 67,413.9 \\ \hline 1,849.9 \times 10^6 + 10,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 3,311,770 \quad 1,098 \quad 28.26 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,221,160 \\ \hline - 2,450,267 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

$$\begin{array}{r} \text{Same as volume flow (acfm) except adjusted for standard temperature of} \\ 68^\circ\text{F} \\ 3,311,770 \quad 28.26 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 752,742 \\ \hline - 851,152 \text{ scfm} \end{array}$$

West. 501F
Natural Gas
Base Load
79°F

12018G2/APPA-
06/13/92
8/26/92

Volume Flow from HRSG (acfm):

$$\begin{aligned} & \text{CT Exhaust adjusted for temperature} \\ & 2,221,160 \\ & \cancel{2,450,287} \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + \cancel{1,098} (1,060^\circ\text{F} + 460^\circ\text{F}) \\ & \quad 948,056 \\ & - \cancel{1,072,001} \text{ acfm} \end{aligned}$$

Velocity (ft/sec):

$$\begin{aligned} & \text{Volume Flow (ft}^3\text{/min) + Area (ft}^2\text{) + 60 sec/min} \\ & 948,056 \\ & \cancel{1,072,001} \text{ ft}^3\text{/min} + 60 + (18.0^2 + 4 \times 3.14159) \\ & \quad 62.1 \\ & - \cancel{70.2} \text{ ft/sec} \end{aligned}$$

25
Table A-2:

$$\begin{aligned} & \text{PM emissions in tons per year} \\ & 5.9 \quad 8460 \\ & \cancel{17} \text{ lb/hr} \times \cancel{300} \text{ hr/yr} + 2,000 \text{ lb/ton} \\ & \quad 24.96 \\ & - 2.6 \text{ ton/yr} \end{aligned}$$

$$\begin{aligned} & \text{SO}_2 \text{ Emissions--Oil (lb/hr)} \\ & 1,489,105 \text{ cf/hr} \quad 1.09 \text{ lb/100 cf} \\ & \cancel{99,722.9} \text{ lb/hr} \times \cancel{0.0005} \text{ lb S/lb} \times 2 \text{ lb SO}_2\text{/lb S} \times 1.016/7000 \text{ gr} \\ & \quad 4.24 \\ & - \cancel{99.72} \text{ lb/hr} \end{aligned}$$

NO_x Emissions (lb/hr) - See Note B:

$$\begin{aligned} & 25.5 \quad 9.32 \quad 12.82 \\ & 42 \text{ ppm} \times [20.9 \times (1 - \cancel{11.59}/100) - \cancel{10.96}] \times 2,116.8 \text{ lb/ft}^2 \\ & \quad \times \cancel{2,450,287} \text{ ft}^3\text{/min} \\ & \quad 2,221,160 \\ & \times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times \cancel{1,060}^\circ\text{F} + 460^\circ\text{F}] \\ & \quad \times 5.9 \times 10^6 \text{ (adjust for ppm)} \\ & \quad 142.9 \\ & - \cancel{326.2} \text{ lb/hr} \end{aligned}$$

West 501F
 Natural Gas
 Base Load
 79°F

12018C2/APPA-3
 06/12/92
 8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 10.4 \quad 9.32 \quad 2,221,160 \\
 & 30 \text{ ppm} \times (1 - 11.59/100) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^3 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \quad \quad \quad 1,098 \\
 & \times 60 \text{ min/hr} + (1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) \times 10^6) \\
 & \quad 30.9 \\
 & - 98.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 4.1 \quad 9.32 \quad 2,221,160 \\
 & 3.5 \text{ ppm} \times (1 - 11.59/100) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^3 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \quad \quad \quad 1,098 \\
 & \times 60 \text{ min/hr} + (1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) \times 10^6) \\
 & \quad 6.97 \\
 & - 6.56 \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\cancel{8.0 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr} = 1.65 \times 10^{-2} \text{ lb/hr}}$$

²⁶
 Table A-2:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned}
 & (1,483,105 \text{ cf/hr} \times 1.09 \text{ lb}/100 \text{ cf} \times 2 \text{ lb SO}_2 / \text{lb S} \times 1.016 / 7000 \text{ cf}) \quad 0.08 \\
 & \cancel{10,722.0 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4 / \text{lb SO}_2 \times 0.05} \\
 & \quad \text{(converted)} \quad 1.53 \\
 & \quad 0.546 \\
 & - 12.2 \text{ lb/hr}
 \end{aligned}$$

A-26, A-27, A-28:
 Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \cancel{1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu}} \quad \text{Not Applicable} \\
 & \quad - 2.59 \times 10^{-2} \text{ lb/hr}
 \end{aligned}$$

Emission Calculations, Tables A-26, A-27, A-28

Manufacturer/Model: West 501F
 Fuel Type: Natural Gas
 Load: Base
 Ambient Temperature: 79°F

Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1,409.0 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = 1.56 × 10⁻³ lb/hr

Formaldehyde: 88.12 lb/10¹² Btu x 1,409.0 MMBtu/hr + 10⁶ MMBtu/10¹² Btu = 0.129 lb/hr

Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ = NA lb/hr

West 501F
Natural Gas
Base Load
97°F

12018C2/APPA-1
06/13/92
8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ²⁴97°F CONDITIONS

(From Table A-1 On ~~Distillate Oil~~; ²⁴Natural Gas; Base Load)

All Other Calculations on Spreadsheet are Identical.)

²⁴Table A-1: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10^6 Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (} 10^6 \text{ Btu/kWh)} \\ 129,570 \quad 10,360 \quad 1,340.3 \\ 183,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas

~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (} 10^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,340.3 \quad 20,900 \quad 64,127.9 \\ 1,849.9 \times 10^6 + 18,550 - 99,725 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 3,180,510 \quad 1,111 \quad 28.23 \\ 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,152,966 \\ - 2,450,207 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

$$\begin{array}{r} \text{Same as volume flow (acfm) except adjusted for standard temperature of} \\ 68^\circ\text{F} \\ 3,180,510 \quad 28.23 \\ 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 723,594 \\ - 851,152 \text{ scfm} \end{array}$$

West. 501F
 Natural Gas
 Base Load
 97°F

12018G2/APPA-2
~~06/12/92~~
 8/26/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{2,152,966}{2,450,287} \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + \frac{1,111}{1,060} \times (1,060^\circ\text{F} + 460^\circ\text{F})$$

$$= 911,345$$

$$- 1,072,001 \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\frac{911,345}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$= 59.7$$

$$- 70.2 \text{ ft/sec}$$

²⁵
 Table A-4:

PM emissions in tons per year

$$\frac{5.7}{17} \text{ lb/hr} \times \frac{8460}{200} \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$= 24.11$$

$$- 2.6 \text{ ton/yr}$$

Nat. Gas

SO₂ Emissions - Oil (lb/hr)

$$\frac{1,410,814 \text{ cf/hr}}{99,722.9 \text{ lb/hr}} \times \frac{1.09 \text{ gr/100 cf}}{0.0005 \text{ lb S/lb}} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb/7000 gr}$$

$$= 4.03$$

$$- 99.72 \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$\frac{855}{42} \text{ ppm} \times [20.9 \times (1 - \frac{9.56}{100}) - 10.96] \times \frac{12.84}{2,116.8} \text{ lb/ft}^2$$

$$\times \frac{2,152,966}{2,450,287} \text{ ft}^3/\text{min}$$

$$\times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times \frac{1,111}{1,060} \times (1,060^\circ\text{F} + 460^\circ\text{F})$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}]$$

$$= 135.8$$

$$- 326.7 \text{ lb/hr}$$

WEST 501 F
 Natural Gas
 Base Load
 97°F

12018C2/APPA-3
 06/17/92
 8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 10.2 \quad 9.56 \quad 2,152,966 \\
 & 90 \text{ ppm} \times (1 - 11.59/100) \times 2,450,267 \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (1,111 / (1,060^\circ\text{F} + 460^\circ\text{F})) \times 10^6) \\
 & \quad 29.1 \\
 & - 98.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 4.3 \quad 9.56 \quad 2,152,966 \\
 & 3.5 \text{ ppm} \times (1 - 11.59/100) \times 2,450,267 \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (1,111 / (1,060^\circ\text{F} + 460^\circ\text{F})) \times 10^6) \\
 & \quad 7.01 \\
 & - 6.56 \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\cancel{8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr} = 1.63 \times 10^{-2} \text{ lb/hr}}$$

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 Table A-9:

H₂SO₄ Mist Emissions (lb/hr):

$$\begin{aligned}
 & \text{Based on 8 percent of sulfur converted to acid mist} \\
 & (1,410,814 \text{ cf/hr} \times 1.0 \text{ gr}/100 \text{ cf} \times 2.16 \text{ SO}_2/\text{lb S} \times 1.0 \text{ lb}/7000 \text{ cf}) \quad 0.08 \\
 & \cancel{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S}/\text{lb} \times 1.53 \text{ lb H}_2\text{SO}_4/\text{lb SO}_2 \times 0.05} \\
 & \quad \text{(converted)} \\
 & \quad 0.520 \\
 & - 12.2 \text{ lb/hr}
 \end{aligned}$$

A-26, A-27, A-28:
 Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & 1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu} \quad \text{Not Applicable} \\
 & - 2.59 \times 10^{-2} \text{ lb/hr}
 \end{aligned}$$

Emission Calculations, Tables A-26 A-27 A-28

Manufacturer/Model: WEST. 501F
Fuel Type: Natural Gas
Load: Base
Ambient Temperature: 97°F

- Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1340.3 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
1.49
- 1.49 x 10⁻³ lb/hr
1340.3
- Formaldehyde: 88.12 lb/10¹² Btu x 1340.3 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.118 lb/hr
- Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ - NA lb/hr

WEST 501 F
DISTILLATE OIL
70% LOAD
27 °F

12018C2/APPA-1
06/13/92
8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - 27°F CONDITIONS

(From Table A-1^{19A} On Distillate Oil; 70% LOAD)

All Other Calculations on Spreadsheet are Identical.)

^{19A}
Table A-1: (Note: all other data not calculated but supplied by
Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 133,020 \quad 9,770 \quad 1,299.6 \\ \hline 1,313,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Fuel Oil (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,299.6 \quad 18,450 \quad 70,439.3 \\ \hline 1,849.9 \times 10^6 + 18,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,934,960 \quad 1,130 \quad 28.34 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 2,003,120 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

$$\begin{array}{r} \text{Same as volume flow (acfm) except adjusted for standard temperature of} \\ 68^\circ\text{F} \\ 2,934,960 \quad 28.34 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 831,404 \\ \hline - 851,152 \text{ scfm} \end{array}$$

WEST 501 F
DISTILLATE OIL
70% LOAD
27°F

12018G2/APPA-2
06/13/92
8/26/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\begin{array}{r} 2,003,120 \quad 200 \quad 1,130 \\ 2,450,287 \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + (1,060^\circ\text{F} + 460^\circ\text{F}) \\ 831,484 \\ - 1,072,001 \text{ acfm} \end{array}$$

Velocity (ft/sec):

$$\begin{array}{r} \text{Volume Flow (ft}^3\text{/min)} + \text{Area (ft}^2\text{)} + 60 \text{ sec/min} \\ 831,484 \\ 1,072,001 \text{ ft}^3\text{/min} + 60 + (18.0^2 + 4 \times 3.14159) \\ 54.5 \\ - 70.2 \text{ ft/sec} \end{array}$$

20A
Table A-2:

PM emissions in tons per year

$$\begin{array}{r} 32.6 \\ 17 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton} \\ 4.9 \\ - 2.6 \text{ ton/yr} \end{array}$$

SO₂ Emissions--Oil (lb/hr)

$$\begin{array}{r} 70,439.3 \\ 99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2\text{/lb S} \\ 72.69 \\ - 99.72 \text{ lb/hr} \end{array}$$

NO_x Emissions (lb/hr) - See Note B:

$$\begin{array}{r} 42.5 \quad 10.43 \quad 12.08 \\ 42 \text{ ppm} \times [20.9 \times (1 - 11.59/100) - 10.96] \times 2,116.8 \text{ lb/ft}^2 \\ \times 2,450,287 \text{ ft}^3\text{/min} \\ 2,003,120 \\ \times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) \\ \times 5.9 \times 10^6 \text{ (adjust for ppm)}] \\ 227.9 \\ - 326.2 \text{ lb/hr} \end{array}$$

WEST 501 F
DISTILLATE OIL
70 % LOAD
27 °F

12018C2/APPA-3
06/12/92
8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned} & 51.5 \quad 10.43 \quad 2,003,120 \\ & 30 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,130} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\ & \quad \text{(molecular wgt. of carbon)} \\ & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,130}{1,060^\circ\text{F}} + 460^\circ\text{F}) \times 10^6) \\ & \quad 133.8 \\ & - 98.4 \text{ lb/hr} \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned} & 10.0 \quad 10.43 \quad 2,003,120 \\ & 3.5 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,130} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\ & \quad \text{(molecular wgt. of methane)} \\ & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,130}{1,060^\circ\text{F}} + 460^\circ\text{F}) \times 10^6) \\ & \quad 14.84 \\ & - 6.56 \text{ lb/hr} \end{aligned}$$

Lead Emissions (lb/hr):

$$8.9 \text{ lb}/10^{12} \text{ Btu} \times \frac{1,299.6}{1,849.9} \times 10^6 \text{ Btu/hr} - \frac{1.16}{1.65} \times 10^{-2} \text{ lb/hr}$$

21A

Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned} & 70,439.3 \\ & \frac{99,722.9}{8} \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb S} \times 0.08 \\ & \quad \text{(converted)} \\ & \quad 8.90 \\ & - 12.2 \text{ lb/hr} \end{aligned}$$

22A

Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned} & 1,299.6 \\ & \frac{1,849.9}{1.82} \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu} \\ & - 2.59 \times 10^{-2} \text{ lb/hr} \end{aligned}$$

7/27/92
8/26/92

Emission Calculations, Tables A-21A, A-22A, A-23A

Manufacturer/Model: WEST. 501F
Fuel Type: Distillate Oil
Load: 70%
Ambient Temperature: 27°F

- Arsenic: 4.2 lb/10¹² Btu x ^{1299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{5.46}~~5.59~~ × 10⁻³ lb/hr
- Beryllium: 2.5 lb/10¹² Btu x ^{1299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{3.25}~~3.38~~ × 10⁻³ lb/hr
- Mercury: 3.0 lb/10¹² Btu x ^{1299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{3.90}~~4.0~~ × 10⁻³ lb/hr
- Fluoride: 14.0 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{1,299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{4.23}~~4.33~~ × 10⁻² lb/hr
- Nickel: 170 lb/10¹² Btu x ^{1,299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{0.226}~~0.23~~ lb/hr
- Cadmium: 10.5 lb/10¹² Btu x ^{1,299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{1.36}~~1.4~~ × 10⁻² lb/hr
- Chromium: 47.5 lb/10¹² Btu x ^{1,299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{6.17}~~6.3~~ × 10⁻² lb/hr
- Copper: 280 lb/10¹² Btu x ^{1,299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{0.364}~~0.37~~ lb/hr
- Vanadium: 69.5 lb/10¹² Btu x ^{1,299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{9.03}~~9.2~~ × 10⁻² lb/hr
- Selenium: 23.42 lb/10¹² Btu x ^{1,299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{3.04}~~3.12~~ × 10⁻² lb/hr
- Polycyclic Organic Matter: 0.278 lb/10¹² Btu x ^{1,299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{3.61}~~3.7~~ × 10⁻⁴ lb/hr
- Formaldehyde: 405 lb/10¹² Btu x ^{1,299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{0.526}~~0.53~~ lb/hr
- Antimony: 9.4 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{1,299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{2.84}~~2.9~~ × 10⁻² lb/hr
- Barium: 8.4 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{1,299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{2.54}~~2.6~~ × 10⁻² lb/hr
- Cobalt: 3.9 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{1,299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{1.18}~~1.2~~ × 10⁻² lb/hr
- zinc: 294 pg/J x 2.324 lb/10¹² Btu/pg/J x ^{1,299.6}~~1331~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - ^{0.883}~~0.9~~ lb/hr
- Chlorine: 0.5 ppm x ^{70,437.3}~~73,500~~ lb/hr fuel oil + 10⁶ - ^{3.52}~~3.6~~ × 10⁻² lb/hr

WEST 501 F
DISTILLATE OIL
70% LOAD
72°F

12018C2/APPA-1

06/13/92

8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁷²27°F CONDITIONS

(From Table A-^{19A}1 On Distillate Oil; 70% LOAD)

All Other Calculations on Spreadsheet are Identical.)

^{19A}Table A-1: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10^6 Btu/hr):

$$\begin{aligned} &\text{Power (kW)} \times \text{Heat Rate (}10^6 \text{ Btu/kWh)} \\ &113,400 \quad 10,310 \quad 1,169.2 \\ &183,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{aligned}$$

Fuel Oil (lb/hr):

$$\begin{aligned} &\text{Heat Input (}10^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ &1,169.2 \quad 18,450 \quad 63,368.8 \\ &1,849.9 \times 10^6 + 18,550 - 99,723 \text{ lb/hr} \end{aligned}$$

Volume Flow (acfm) - See Note A:

$$\begin{aligned} V &= mRT/PM \\ &2,757,580 \quad 1,130 \quad 28.19 \\ &3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ &+ 60(\text{min/hr}) \\ &1,892,217 \\ &- 2,450,287 \text{ acfm} \end{aligned}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{aligned} &68^\circ\text{F} \\ &2,757,580 \quad 28.19 \\ &3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ &620,359 \\ &- 851,152 \text{ scfm} \end{aligned}$$

WEST 501 F
DISTILLATE OIL
70% LOAD
72°F

12018C2/APPA-1
06/13/92
2/26/92

Volume Flow from HRSG (acfm):

$$\begin{aligned} & \text{GT Exhaust adjusted for temperature} \\ & \frac{1,892,217}{\cancel{2,450,287}} \times \frac{200}{(205^\circ\text{F} + 460^\circ\text{F})} + \frac{1,130}{(1,060^\circ\text{F} + 460^\circ\text{F})} \\ & \quad 785,449 \\ & - 1,072,001 \text{ acfm} \end{aligned}$$

Velocity (ft/sec):

$$\begin{aligned} & \text{Volume Flow (ft}^3\text{/min)} + \text{Area (ft}^2\text{)} + 60 \text{ sec/min} \\ & \frac{785,449}{1,072,001 \text{ ft}^3\text{/min} + 60} + (18.0^2 + 4 \times 3.14159) \\ & \quad 51.4 \\ & - 70.2 \text{ ft/sec} \end{aligned}$$

20A
Table A-2:

PM emissions in tons per year

$$\begin{aligned} & 30 \\ & \frac{17 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton}}{4.5} \\ & - 2.6 \text{ ton/yr} \end{aligned}$$

SO₂ Emissions--Oil (lb/hr)

$$\begin{aligned} & 43,368.8 \\ & \frac{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2\text{/lb S}}{65.65} \\ & - 99.72 \text{ lb/hr} \end{aligned}$$

NO_x Emissions (lb/hr) - See Note B:

$$\begin{aligned} & 42.5 \quad 11.58 \quad 12.17 \\ & \frac{42 \text{ ppm} \times [20.9 \times (1 - \frac{11.58}{100}) - 10.96] \times 2,116.8 \text{ lb/ft}^2}{\times 2,450,287 \text{ ft}^3\text{/min}} \\ & \quad \quad \quad 1,130 \\ & \times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) \\ & \quad \times 5.9 \times 10^6 \text{ (adjust for ppm)}] \\ & \quad 204.5 \\ & - 326.2 \text{ lb/hr} \end{aligned}$$

WEST 501 F
 DISTILLATE OIL
 70% LOAD
 72°F

12018C2/APPA-3
 06/12/92
 8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned} & \overset{51.5}{30} \text{ ppm} \times \left(1 - \frac{\overset{11.58}{11.59}}{100}\right) \times \overset{1,892,217}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\ & \quad \text{(molecular wgt. of carbon)} \\ & \times 60 \text{ min/hr} + (1,545 \times \overset{1,130}{1,060}^\circ\text{F} + 460^\circ\text{F}) \times 10^6 \\ & \quad \overset{124.7}{- 98.4} \text{ lb/hr} \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned} & \overset{10.1}{3.5} \text{ ppm} \times \left(1 - \frac{\overset{11.58}{11.59}}{100}\right) \times \overset{1,892,217}{2,450,287} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\ & \quad \text{(molecular wgt. of methane)} \\ & \times 60 \text{ min/hr} + (1,545 \times \overset{1,130}{1,060}^\circ\text{F} + 460^\circ\text{F}) \times 10^6 \\ & \quad \overset{13.98}{- 6.56} \text{ lb/hr} \end{aligned}$$

Lead Emissions (lb/hr):

$$8.9 \text{ lb}/10^{12} \text{ Btu} \times \overset{1,169.2}{1,849.9} \times 10^6 \text{ Btu/hr} = \overset{1.04}{1.65} \times 10^{-2} \text{ lb/hr}$$

^{21A}
 Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned} & \overset{63,768.8}{99,722.9} \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb S} \times 0.08 \\ & \quad \text{(converted)} \\ & \quad \overset{8.04}{- 12.2} \text{ lb/hr} \end{aligned}$$

^{22A}
 Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned} & \overset{1,169.2}{1,849.9} \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu} \\ & \quad \overset{1.64}{- 2.59} \times 10^{-2} \text{ lb/hr} \end{aligned}$$

7/27/92
8/26/92

Emission Calculations, Tables A-21A, A-22A, A-23A

Manufacturer/Model: West 501F
Fuel Type: Distillate Oil
Load: 10%
Ambient Temperature: 72°F

Arsenic: 4.2 lb/10¹² Btu x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 4.96 × 10⁻³ lb/hr

Beryllium: 2.5 lb/10¹² Btu x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 2.97 × 10⁻³ lb/hr

Mercury: 3.0 lb/10¹² Btu x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.56 × 10⁻³ lb/hr

Fluoride: 14.0 pg/J x 2.324 lb/10¹² Btu/pg/J x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.80 × 10⁻² lb/hr

Nickel: 170 lb/10¹² Btu x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.199 lb/hr

Cadmium: 10.5 lb/10¹² Btu x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 1.23 × 10⁻² lb/hr

Chromium: 47.5 lb/10¹² Btu x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 5.55 × 10⁻² lb/hr

Copper: 280 lb/10¹² Btu x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.327 lb/hr

Vanadium: 69.5 lb/10¹² Btu x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 8.13 × 10⁻² lb/hr

Selenium: 23.42 lb/10¹² Btu x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 2.76 × 10⁻² lb/hr

Polycyclic Organic Matter: 0.278 lb/10¹² Btu x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 3.25 × 10⁻⁴ lb/hr

Formaldehyde: 405 lb/10¹² Btu x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.474 lb/hr

Antimony: 9.4 pg/J x 2.324 lb/10¹² Btu/pg/J x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 2.55 × 10⁻² lb/hr

Barium: 8.4 pg/J x 2.324 lb/10¹² Btu/pg/J x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 2.28 × 10⁻² lb/hr

Cobalt: 3.9 pg/J x 2.324 lb/10¹² Btu/pg/J x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 1.08 × 10⁻² lb/hr

Zinc: 294 pg/J x 2.324 lb/10¹² Btu/pg/J x $\frac{69.2}{11800}$ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.799 lb/hr

Chlorine: 0.5 ppm x $\frac{63,368.8}{65,354.6}$ lb/hr fuel oil + 10⁶ - 3.17 × 10⁻² lb/hr

WEST 501 F
DISTILLATE OIL
70% LOAD
97 ° F

12018C2/APPA-1
06/13/92
8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁹⁷27 ° F CONDITIONS

(From Table A-1^{19A} On Distillate Oil; 70% LOAD)

All Other Calculations on Spreadsheet are Identical.)

^{19A}
Table A-1: (Note: all other data not calculated but supplied by
Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 102,810 \quad 10,680 \quad 1,098 \\ 102,810 \times 10,680/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Fuel Oil (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,098 \quad 18,450 \quad 59,512.8 \\ 1,849.9 \times 10^6 + 18,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,662,180 \quad 1,130 \quad 28.12 \\ 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 1,831,107 \\ - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

$$\begin{array}{r} \text{Same as volume flow (acfm) except adjusted for standard temperature of} \\ 68^\circ\text{F} \\ 2,662,180 \quad 28.12 \\ 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 608,066 \\ - 851,152 \text{ scfm} \end{array}$$

WEST 501 F
 DISTILLATE OIL
 70% LOAD
 97 °F

12018C2/APPA-2
 06/13/92
 8/26/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\begin{aligned}
 & 1,831,107 \quad 200 \quad 1,130 \\
 & \cancel{2,450,287} \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + (\cancel{1,060}^\circ\text{F} + 460^\circ\text{F}) \\
 & \quad 760,082 \\
 & = \cancel{1,072,001} \text{ acfm}
 \end{aligned}$$

Velocity (ft/sec):

$$\begin{aligned}
 & \text{Volume Flow (ft}^3\text{/min)} \div \text{Area (ft}^2\text{)} \div 60 \text{ sec/min} \\
 & \quad 760,082 \\
 & \cancel{1,072,001} \text{ ft}^3\text{/min} \div 60 \div (18.0^2 + 4 \times 3.14159) \\
 & \quad 49.8 \\
 & = \cancel{70.2} \text{ ft/sec}
 \end{aligned}$$

20A
 Table A-2:

PM emissions in tons per year

$$\begin{aligned}
 & 28.5 \\
 & \cancel{17} \text{ lb/hr} \times 300 \text{ hr/yr} \div 2,000 \text{ lb/ton} \\
 & \quad 4.3 \\
 & = \cancel{2.6} \text{ ton/yr}
 \end{aligned}$$

SO₂ Emissions--Oil (lb/hr)

$$\begin{aligned}
 & 59,512.8 \\
 & \cancel{99,722.9} \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2\text{/lb S} \\
 & \quad 61.77 \\
 & = \cancel{99.72} \text{ lb/hr}
 \end{aligned}$$

NO_x Emissions (lb/hr) - See Note B:

$$\begin{aligned}
 & 42.7 \quad 12.09 \quad 12.26 \\
 & \cancel{42} \text{ ppm} \times [20.9 \times (1 - \cancel{11.59}/100) - \cancel{10.96}] \times 2,116.8 \text{ lb/ft}^2 \\
 & \quad \times \cancel{2,450,287} \text{ ft}^3\text{/min} \\
 & \quad \quad 1,831,107 \quad 1,130 \\
 & \times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times (\cancel{1,060}^\circ\text{F} + 460^\circ\text{F}) \\
 & \quad \times 5.9 \times 10^6 \text{ (adjust for ppm)}] \\
 & \quad 192.7 \\
 & = \cancel{326.2} \text{ lb/hr}
 \end{aligned}$$

WEST 501 F
 DISTILLATE OIL
 70% LOAD
 97 °F

12018C2/APPA-3
 06/12/92
 8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 51.5 \quad 12.09 \quad 1,831,107 \\
 & -30 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,130} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,130}{1,060} \text{ °F} + 460 \text{ °F}) \times 10^6) \\
 & \quad 120.0 \\
 & - 98.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 10.5 \quad 12.09 \quad 1,831,107 \\
 & -3.5 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,130} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,130}{1,060} \text{ °F} + 460 \text{ °F}) \times 10^6) \\
 & \quad 13.98 \\
 & - 6.56 \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr):

$$\begin{aligned}
 & 8.9 \text{ lb/10}^{12} \text{ Btu} \times \frac{1098}{1,849.9} \times 10^6 \text{ Btu/hr} - \frac{9.77}{1.65} \times 10^{-2} \text{ lb/hr}
 \end{aligned}$$

21A
 Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned}
 & 59,512.8 \\
 & 99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb S} \times 0.08 \\
 & \quad \text{(converted)} \\
 & \quad 7.57 \\
 & - 12.2 \text{ lb/hr}
 \end{aligned}$$

22A
 Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & 1098 \\
 & 1,849.9 \text{ (MMBtu)} \times 14 \text{ lb/10}^{12} \text{ Btu} \\
 & \quad 1.54 \\
 & - 2.59 \times 10^{-2} \text{ lb/hr}
 \end{aligned}$$

Emission Calculations, Tables A-21A, A-22A, A-23A

Manufacturer/Model: West. 501F
 Fuel Type: Distillate Oil
 Load: 70%
 Ambient Temperature: 97°F

- Arsenic: 4.2 lb/10¹² Btu x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu ^{4.61}~~4.61~~⁻³ lb/hr
- Beryllium: 2.5 lb/10¹² Btu x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu ^{2.74}~~2.74~~⁻³ lb/hr
- Mercury: 3.0 lb/10¹² Btu x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu ^{3.29}~~3.29~~⁻³ lb/hr
- Fluoride: 14.0 pg/J x 2.324 lb/10¹² Btu/pg/J x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
^{3.57}~~3.57~~⁻² lb/hr
- Nickel: 170 lb/10¹² Btu x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = ^{0.187}~~0.187~~ lb/hr
- Cadmium: 10.5 lb/10¹² Btu x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = ^{1.17}~~1.17~~⁻² lb/hr
- Chromium: 47.5 lb/10¹² Btu x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = ^{5.22}~~5.22~~⁻² lb/hr
- Copper: 280 lb/10¹² Btu x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = ^{0.707}~~0.707~~ lb/hr
- Vanadium: 69.5 lb/10¹² Btu x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = ^{7.63}~~7.63~~⁻² lb/hr
- Selenium: 23.42 lb/10¹² Btu x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = ^{2.57}~~2.57~~⁻² lb/hr
- Polycyclic Organic Matter: 0.278 lb/10¹² Btu x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
^{3.05}~~3.05~~⁻⁴ lb/hr
- Formaldehyde: 405 lb/10¹² Btu x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = ^{0.445}~~0.445~~ lb/hr
- Antimony: 9.4 pg/J x 2.324 lb/10¹² Btu/pg/J x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
^{2.41}~~2.41~~⁻² lb/hr
- Barium: 8.4 pg/J x 2.324 lb/10¹² Btu/pg/J x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
^{2.17}~~2.17~~⁻² lb/hr
- Cobalt: 3.9 pg/J x 2.324 lb/10¹² Btu/pg/J x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
^{9.15}~~9.15~~⁻³ lb/hr
- Zinc: 294 pg/J x 2.324 lb/10¹² Btu/pg/J x ¹⁰⁹⁸~~1164~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
^{0.750}~~0.750~~ lb/hr
- Chlorine: 0.5 ppm x ^{59,512.8}~~61,621~~ lb/hr fuel oil + 10⁶ ^{2.98}~~2.98~~⁻² lb/hr

West. 501F
 Natural Gas
 70% LOAD
 27°F

12018C2/APPA-1
 06/13/92
 8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ²⁷F CONDITIONS

(From Table A-^{24A} On ~~Distillate Oil~~; ^{Natural Gas} 70% LOAD)

All Other Calculations on Spreadsheet are Identical.)

^{24A}
 Table A-~~5~~: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10^6 Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (} 10^6 \text{ Btu/kWh)} \\ 118,330 \quad 10,470 \quad 1,241.3 \\ \hline 1,837,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas
~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (} 10^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,241.3 \quad 20,900 \quad 59,391.5 \\ \hline 1,849.9 \times 10^6 + 10,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,754,000 \quad 1,130 \quad 28.49 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,080^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 1,869,744 \\ \hline - 2,450,267 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68^\circ\text{F} \\ 2,754,000 \quad 28.49 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 620,896 \\ \hline - 851,152 \text{ scfm} \end{array}$$

West. 501F
 Natural Gas
 70% LOAD
 27°F

12018G2/APPA-;
 06/23/92
 8/26/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{1,869,744}{2,450,287} \text{ acfm} \times \frac{200}{(200^\circ\text{F} + 460^\circ\text{F})} + \frac{1,130}{(1,060^\circ\text{F} + 460^\circ\text{F})}$$

$$= \frac{776,120}{1,072,001} \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\frac{776,120}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$= \frac{50.8}{70.2} \text{ ft/sec}$$

25A
 Table A-2:

PM emissions in tons per year

$$\frac{4.9}{17} \text{ lb/hr} \times \frac{8460}{300} \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$= \frac{20.73}{2.6} \text{ ton/yr}$$

GAS
 SO₂ Emissions - ~~0.1~~ (lb/hr)

$$\frac{1,306,612 \text{ cf/hr}}{99,722.9 \text{ lb/hr}} \times \frac{1.09 \text{ g/100cf}}{0.0005 \text{ lb S/lb}} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb/7000g}$$

$$= \frac{3.73}{99.72} \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$\frac{25.4}{42} \text{ ppm} \times \left[\frac{7.30}{20.9} \times \left(1 - \frac{11.59}{100} \right) - \frac{13.04}{10.96} \right] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{1,869,744}{2,450,287} \text{ ft}^3/\text{min}$$

$$\times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + \left[1,545 \times \frac{1,130}{(1,060^\circ\text{F} + 460^\circ\text{F})} \right]$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$= \frac{121.3}{326.2} \text{ lb/hr}$$

West 301F
Natural Gas
70% Load
27°F

12018C2/APPA-3
~~06/12/92~~
8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned} & 10.4 \quad 7.3 \quad 1,869,744 \\ & 30 \text{ ppm} \times (1 - 11.59/100) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\ & \quad \text{(molecular wgt. of carbon)} \\ & \quad \quad \quad 1,130 \\ & \times 60 \text{ min/hr} + (1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) \times 10^6) \\ & \quad 26.1 \\ & - 98.4 \text{ lb/hr} \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned} & 4.2 \quad 7.3 \quad 1,869,744 \\ & 2.5 \text{ ppm} \times (1 - 11.59/100) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\ & \quad \text{(molecular wgt. of methane)} \\ & \quad \quad \quad 1,130 \\ & \times 60 \text{ min/hr} + (1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) \times 10^6) \\ & \quad 6.02 \\ & - 6.56 \text{ lb/hr} \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\cancel{8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr} = 1.65 \times 10^{-2} \text{ lb/hr}}$$

^{26A}
Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned} & 1,306,612 \text{ cf/hr} \times 109 \text{ lb}/100 \text{ cf} \times 216 \text{ SO}_2 / 165 \times 1.0 \text{ lb}/7000 \text{ gr} \quad 0.08 \\ & \quad \quad \quad 99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2.86 \text{ lb H}_2\text{SO}_4 / \text{lb SO}_2 \times 0.05 \\ & \quad \quad \quad \text{(converted)} \quad \quad \quad 1.53 \\ & \quad \quad \quad 0.481 \\ & - 12.2 \text{ lb/hr} \end{aligned}$$

A-26A, A-27A, A-28A
Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned} & 1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu} \quad \text{Not Applicable} \\ & \quad \quad \quad 2.59 \times 10^{-2} \text{ lb/hr} \end{aligned}$$

7/31/92

Emission Calculations, Tables A-26A A-27A A-28AManufacturer/Model: WEST 501FFuel Type: NATURAL GASLoad: 70%Ambient Temperature: 27°FArsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hrBeryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hrMercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hrFluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hrNickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hrCadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hrChromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hrCopper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hrVanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hrSelenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hrPolycyclic Organic Matter: 1.113 lb/10¹² Btu x ~~1241.3~~ MMBtu/hr + 10⁶ MMBtu/10¹² Btu- 1.38 × 10⁻³ lb/hrFormaldehyde: 88.12 lb/10¹² Btu x 1241.3 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.109 lb/hrAntimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu- NA lb/hrBarium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu- NA lb/hrCobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu- NA lb/hrZinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu- NA lb/hrChlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ - NA lb/hr

West 301F
Natural Gas
70% Load
64°F

12018C2/APPA-1
06/13/92
8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁶⁴°F CONDITIONS

(From Table A-1 On ^{24A} ~~Distillate Oil~~; ^{Natural Gas} 70% LOAD)

All Other Calculations on Spreadsheet are Identical.)

^{24A}
Table A-1: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10^6 Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (} 10^6 \text{ Btu/kWh)} \\ 103,390 \quad 11,020 \quad 1,139.4 \\ \hline 1,849.9 \times 10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas

~~Fuel Oil~~ (lb/hr):

$$\begin{array}{r} \text{Heat Input (} 10^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,139.4 \quad 20,900 \quad 54,514.7 \\ \hline 1,849.9 \times 10^6 + 18,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = \frac{mRT}{PM} \\ 2,678,720 \quad 1,130 \quad 28.36 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (\frac{1,130}{2,000} \text{°F} + 460 \text{°F}) + (28.36 \times 2,116.8 \text{ lb/ft}^2) \\ + 60 \text{ (min/hr)} \\ 1,926,635 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68 \text{°F} \\ 2,678,720 \quad 28.36 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68 \text{°F} + 460 \text{°F}) + (28.36 \times 2,116.8) + 60 \\ 606,581 \\ \hline - 851,152 \text{ scfm} \end{array}$$

West 501F
 Natural Gas
 70% Load
 64°F

12018C2/APPA-;
 06/13/92
 8/26/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{1,826,635}{2,450,287} \text{ acfm} \times \frac{200}{(205^\circ\text{F} + 460^\circ\text{F})} + \frac{1,130}{(1,060^\circ\text{F} + 460^\circ\text{F})}$$

$$= 758,226 - 1,072,001 \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\frac{758,226}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$= 49.7 - 70.2 \text{ ft/sec}$$

25A
 Table A-5:

PM emissions in tons per year

$$\frac{4.8}{17} \text{ lb/hr} \times \frac{8460}{300} \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$= 20.30 - 2.6 \text{ ton/yr}$$

GAS
 SO₂ Emissions - Oil (lb/hr)

$$\frac{1,199,324 \text{ cf/hr}}{99,722.9 \text{ lb/hr}} \times \frac{1.09 \text{ lb}}{100 \text{ cf}} \times 2 \text{ lb SO}_2/\text{lb s} \times \frac{1.016}{7000} \text{ gr}$$

$$= 3.43 - 99.72 \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$\frac{25.4}{42} \text{ ppm} \times [20.9 \times (1 - \frac{8.32}{100}) - \frac{13.1}{10.96}] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{1,826,635}{2,450,287} \text{ ft}^3/\text{min}$$

$$\times 46 \text{ (molecular wgt NO}_2) \times 60 \text{ min/hr} + [1,545 \times \frac{1,130}{(1,060^\circ\text{F} + 460^\circ\text{F})}]$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$= 113.4 - 326.2 \text{ lb/hr}$$

West. 501F
 Natural Gas
 70% Load
 64°F

12018G2/APPA-3
 06/22/92
 8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 10.3 \quad 8.32 \quad 1,826,635 \\
 & \text{ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,130} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,060}{1,130} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad 25.0 \\
 & - 98.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 4.3 \quad 8.32 \quad 1,826,635 \\
 & \text{ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,130} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,060}{1,130} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad 5.96 \\
 & - 6.56 \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\cancel{8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr} = 1.65 \times 10^{-2} \text{ lb/hr}}$$

^{26A}
 Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

$$\begin{aligned}
 & \text{Based on 8 percent of sulfur converted to acid mist} \\
 & \underbrace{1,199,324 \text{ cf/hr} \times 1.0 \text{ gr}/100 \text{ cf} \times 2 \text{ lb SO}_2 / \text{lb S} \times 1.0 \text{ lb}/7000 \text{ gr}}_{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times \frac{2.06 \text{ lb H}_2\text{SO}_4 / \text{lb SO}_2 \times 0.08}{1.53}} \\
 & \quad 0.442 \\
 & - 12.7 \text{ lb/hr}
 \end{aligned}$$

A-26A, A-27A, A-28A
 Tables ~~A-4 and A-5~~:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \cancel{1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu}} \quad \text{Not Applicable} \\
 & - \cancel{2.59 \times 10^{-2} \text{ lb/hr}}
 \end{aligned}$$

7/31/92

Emission Calculations, Tables A-26A, A-27A, A-28A

Manufacturer/Model: West 501F
Fuel Type: NATURAL GAS
Load: 70%
Ambient Temperature: 64°F

- Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1139.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- 1.26 × 10⁻³ lb/hr
- Formaldehyde: 88.12 lb/10¹² Btu x 1139.4 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 0.10 lb/hr
- Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ - NA lb/hr

West 501F
Nat Gas
70% Load
72°F

12018C2/APPA-1
~~06/13/92~~
8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁷²°F CONDITIONS

(From Table A-1 On ^{24A} ~~Distillate Oil~~, ^{Nat Gas} 70% Load)

All Other Calculations on Spreadsheet are Identical.)

24A

Table A-1: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10^6 Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (} 10^6 \text{ Btu/kWh)} \\ 100,210 \quad 11,150 \quad 1,117.3 \\ \hline 1,027,700 \times 10,070/10^6 - 1,849.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas

Fuel Oil (lb/hr):

$$\begin{array}{r} \text{Heat Input (} 10^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,117.3 \quad 20,900 \quad 53,461.3 \\ \hline 1,849.9 \times 10^6 + 18,550 - 99,725 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,647,790 \quad 1,130 \quad 28.33 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 1,807,837 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68^\circ\text{F} \\ 2,647,790 \quad 28.33 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 600,338 \\ \hline - 851,152 \text{ scfm} \end{array}$$

Unit 501F
 Nat Gas
 70% Load
 72°F

12018G2/APPA-1
 06/23/92
 8/26/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{1,807,837}{2,450,287} \text{ acfm} \times \left(\frac{200}{200 + 460} \right) + \frac{1,130}{1,060} \text{ acfm} \times \left(\frac{1,130}{1,060 + 460} \right)$$

$$= 750,423 - 1,072,001 \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\frac{750,423}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$= 49.1 - 70.2 \text{ ft/sec}$$

25A

Table A-9:

PM emissions in tons per year

$$4.7 \text{ lb/hr} \times 8460 \text{ hr/yr} + 2,000 \text{ lb/ton}$$

$$= 19.88 - 2.6 \text{ ton/yr}$$

GAS

SO₂ Emissions (lb/hr)

$$\frac{1,176,149 \text{ cf/hr}}{99,722.9} \times 1.09 \text{ lb/100cf} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb/7000 gr}$$

$$= 336 - 99.72 \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$25.4 \text{ ppm} \times \left[20.9 \times \left(1 - \frac{8.68}{100} \right) - 13.08 \right] \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{1,807,837}{2,450,287} \text{ ft}^3/\text{min}$$

$$\times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} + [1,545 \times \frac{1,130}{1,060} \text{ (adjust for ppm)}]$$

$$= 111.2 - 326.2 \text{ lb/hr}$$

West 501F
Nat. Gas
70% Load
72°F

12018C2/APPA-3
~~06/12/92~~
8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned} & \frac{10.4}{30} \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{8.68}{2,450,207} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\ & \quad \text{(molecular wgt. of carbon)} \\ & \times 60 \text{ min/hr} + (1,545 \times \frac{1,130}{1,060^\circ\text{F} + 460^\circ\text{F}} \times 10^6) \\ & \quad - \frac{24.9}{98.4} \text{ lb/hr} \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned} & \frac{4.4}{3.5} \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{8.68}{2,450,207} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\ & \quad \text{(molecular wgt. of methane)} \\ & \times 60 \text{ min/hr} + (1,545 \times \frac{1,130}{1,060^\circ\text{F} + 460^\circ\text{F}} \times 10^6) \\ & \quad - \frac{6.01}{6.56} \text{ lb/hr} \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\frac{8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr}}{1.65 \times 10^{-2} \text{ lb/hr}}$$

^{26A}
Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\frac{1,176,149 \text{ cf/hr} \times 1.09 \text{ lb}/100 \text{ cf} \times 216 \text{ SO}_2/\text{lb S} \times 1.0 \text{ lb}/7000 \text{ gr}}{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4/\text{lb SO}_2 \times 0.05}$$

(converted) 1.53 0.08

$$\frac{0.433}{12.2} \text{ lb/hr}$$

A-26A, A-27A, A-28A
Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\frac{1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu}}{2.59 \times 10^{-2} \text{ lb/hr}} \quad \text{Not Applicable}$$

7/31/92

Emission Calculations, Tables A-26A, A-27A, A-28AManufacturer/Model: West 501FFuel Type: Natural GasLoad: 70%Ambient Temperature: 72°FArsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrBeryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrMercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrFluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hrNickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrCadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrChromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrCopper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrVanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrSelenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hrPolycyclic Organic Matter: 1.113 lb/10¹² Btu x 1113.3 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= 1.24 × 10⁻³ lb/hrFormaldehyde: 88.12 lb/10¹² Btu x 1113.3 MMBtu/hr + 10⁶ MMBtu/10¹² Btu = 9.82 × 10⁻² lb/hrAntimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hrBarium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hrCobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hrZinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hrChlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ = NA lb/hr

Unit 301F
 Natural Gas
 70% Load
 79°F

12018C2/APPA-1
 06/13/92
 8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - 79°F CONDITIONS

(From Table A-1 On ~~Distillate Oil~~; ^{24A} Natural Gas; 70% Load)

All Other Calculations on Spreadsheet are Identical.)

^{24A}
 Table A-1: (Note: all other data not calculated but supplied by
 Manufacturer)

Heat Input (10⁶ Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 97,490 \quad 11,270 \quad 1,098.7 \\ \hline 1,098,700 \times 10,070/10^6 - 1,049.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Natural Gas

Fuel Oil (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,098.7 \quad 20,900 \quad 52,570 \\ \hline 1,049.9 \times 10^6 + 18,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,619,850 \quad 1,130 \quad 28.27 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (20.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 1,792,201 \\ \hline - 2,450,287 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68^\circ\text{F} \\ 2,619,850 \quad 28.27 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (20.25 \times 2,116.8) + 60 \\ 595,146 \\ \hline - 851,152 \text{ scfm} \end{array}$$

Unit 501F
 Natural Gas
 70% Load
 79°F

12018C2/APPA-2
 06/13/92
 8/26/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature
 $1,792,201$
 $2,450,287 \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + (1,130 \times (1,060^\circ\text{F} + 460^\circ\text{F}))$
 $- 1,072,001 \text{ acfm}$
 $743,932$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min
 $743,932$
 $1,072,001 \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$
 48.7
 $- 70.2 \text{ ft/sec}$

25A

Table A-1:

PM emissions in tons per year
 4.7
 $47 \text{ lb/hr} \times 300 \text{ hr/yr} + 2,000 \text{ lb/ton}$
 19.88
 $- 2.6 \text{ ton/yr}$

GAS

SO₂ Emissions - ~~air~~ (lb/hr)
 $1,156,539 \text{ cf/hr}$
 $99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb/7000 gr}$
 3.30
 $- 99.72 \text{ lb/hr}$

NO_x Emissions (lb/hr) - See Note B:

25.4
 $42 \text{ ppm} \times [20.9 \times (1 - \frac{9.12}{100}) - 13.04] \times 2,116.8 \text{ lb/ft}^2$
 $\times 2,450,287 \text{ ft}^3/\text{min}$
 $1,792,201$
 $\times 46 \text{ (molecular wgt NO}_2) \times 60 \text{ min/hr} + [1,545 \times (1,130 \times (1,060^\circ\text{F} + 460^\circ\text{F}))$
 $\times 5.9 \times 10^6 \text{ (adjust for ppm)}]$
 1093
 $- 326.2 \text{ lb/hr}$

West 501F
 Natural Gas
 70% Load
 79°F

12018C2/APPA-3

06/12/92

8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 10.2 \quad 9.12 \quad 1,792,201 \\
 & 99 \text{ ppm} \times (1 - \frac{11.59}{100}) \times 2,450,267 \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \quad \quad \quad 1,130 \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,060}{1,060} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad 24.1 \\
 & - 98.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 4.5 \quad 9.12 \quad 1,792,201 \\
 & 9.5 \text{ ppm} \times (1 - \frac{11.59}{100}) \times 2,450,267 \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \quad \quad \quad 1,130 \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,060}{1,060} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad 6.06 \\
 & - 6.56 \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\frac{8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr}}{1.65 \times 10^{-2} \text{ lb/hr}}$$

26A
 Table A-5:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$$\begin{aligned}
 & (1,156,539 \text{ cf/hr} \times \frac{1.09 \text{ lb}}{100 \text{ cf}} \times \frac{2.1 \text{ lb SO}_2}{\text{lb S}} \times \frac{1.0 \text{ lb}}{7000 \text{ gr}}) \\
 & \quad \frac{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb}}{1.53} \times \frac{3.06 \text{ lb H}_2\text{SO}_4}{\text{lb SO}_2} \times 0.05 \\
 & \quad \quad \quad \text{(converted)} \\
 & \quad 0.426 \\
 & - 12.2 \text{ lb/hr}
 \end{aligned}$$

A-26A, A-27A, A-28A

Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \frac{1,849.9 \text{ (MnBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu}}{2.59 \times 10^{-2} \text{ lb/hr}} \quad \text{Not Applicable} \\
 & - 2.59 \times 10^{-2} \text{ lb/hr}
 \end{aligned}$$

Emission Calculations, Tables A-26A, A-27A, A-28A

Manufacturer/Model: West. 501F
Fuel Type: Natural Gas
Load: 70%
Ambient Temperature: 79°F

- Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Polycyclic Organic Matter: 1.113 lb/10¹² Btu x ~~1098.7~~ ^{1098.7} MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- 1.22x10⁻³ lb/hr
- Formaldehyde: 88.12 lb/10¹² Btu x ~~1098.7~~ ^{1098.7} MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 9.68x10⁻² lb/hr
- Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
- NA lb/hr
- Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ - NA lb/hr

Unit 501F
Natural Gas
70% Load
97°F

12018G2/APPA-1
06/13/92
8/26/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT

EXAMPLE CALCULATIONS - ⁹⁷°F CONDITIONS

(From Table A-1 On ~~Distillate Oil~~; ^{24A} Natural Gas; 70% LOAD)

All Other Calculations on Spreadsheet are Identical.)

24A

Table A-1: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10^6 Btu/hr):

$$\begin{array}{r} \text{Power (kW)} \times \text{Heat Rate (10}^6 \text{ Btu/kWh)} \\ 90,340 \quad 11,600 \quad 1,047.9 \\ \hline 1,047,900 \times 10^6 - 1,049.9 \times 10^6 \text{ Btu/hr} \end{array}$$

Nat. Gas

Fuel Oil (lb/hr):

$$\begin{array}{r} \text{Heat Input (10}^6 \text{ Btu/hr)} + \text{Fuel Heat Content (Btu/lb)} \\ 1,047.9 \quad 20,900 \quad 50,140.9 \\ \hline 1,049.9 \times 10^6 + 10,550 - 99,723 \text{ lb/hr} \end{array}$$

Volume Flow (acfm) - See Note A:

$$\begin{array}{r} V = mRT/PM \\ 2,554,960 \quad 1,130 \quad 28.25 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8 \text{ lb/ft}^2) \\ + 60(\text{min/hr}) \\ 1,749,383 \\ \hline - 2,450,267 \text{ acfm} \end{array}$$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

$$\begin{array}{r} 68^\circ\text{F} \\ 2,554,960 \quad 28.25 \\ \hline 3,743,000 \text{ lb/hr} \times 1,545 \times (68^\circ\text{F} + 460^\circ\text{F}) + (28.25 \times 2,116.8) + 60 \\ 580,927 \\ \hline - 851,152 \text{ scfm} \end{array}$$

Wht 501F
 Natural Gas
 70% Load
 97°F

12018C2/APPA-2
 06/23/92
 8/26/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature
 $1,749,383$ 200 $1,130$
 $2,450,287$ acfm x $(205^\circ\text{F} + 460^\circ\text{F}) + (1,060^\circ\text{F} + 460^\circ\text{F})$
 $- 1,072,001$ acfm
 $726,159$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min
 $726,159$
 $1,072,001$ ft³/min + 60 + $(18.0^2 + 4 \times 3.14159)$
 47.6
 $- 70.2$ ft/sec

25A

Table A-9:

PM emissions in tons per year
 4.6 8460
 17 lb/hr x 500 hr/yr + 2,000 lb/ton
 19.46
 $- 2.6$ ton/yr

GAS

SO₂ Emissions - ~~OTI~~ (lb/hr)
 $1,103,099$ cf/hr 1.09 / 100 cf
 $99,722.9$ lb/hr x 0.0005 lb S/lb x 2 lb SO₂/lb S x 1.0 lb/7000 gr
 3.15
 $- 99.72$ lb/hr

NO_x Emissions (lb/hr) - See Note B:

25.4 9.29 13.15
 42 ppm x $[20.9 \times (1 - \frac{11.59}{100}) - 10.96]$ x $2,116.8$ lb/ft²
x $2,450,287$ ft³/min
 $1,749,383$
x 46 (molecular wgt NO₂) x 60 min/hr + $[1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F})$
x 5.9×10^6 (adjust for ppm)]
 104.0
 $- 226.2$ lb/hr

Unit 501F
 Natural Gas
 70% Load
 97°F

12018C2/APPA-3
~~06/12/92~~
 8/26/92

CO Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 10.4 \quad 9.29 \quad 1,749,383 \\
 & 30 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,130} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 28 \\
 & \quad \text{(molecular wgt. of carbon)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,060}{1,130} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad 23.9 \\
 & - 98.4 \text{ lb/hr}
 \end{aligned}$$

VOC Emissions (lb/hr) - See Note C:

$$\begin{aligned}
 & 3.8 \quad 9.29 \quad 1,749,383 \\
 & 3.5 \text{ ppm} \times (1 - \frac{11.59}{100}) \times \frac{2,450,287}{1,130} \text{ acfm} \times 2,116.8 \text{ lb/ft}^2 \times 16 \\
 & \quad \text{(molecular wgt. of methane)} \\
 & \times 60 \text{ min/hr} + (1,545 \times (\frac{1,060}{1,130} \text{°F} + 460 \text{°F}) \times 10^6) \\
 & \quad 4.99 \\
 & - 6.56 \text{ lb/hr}
 \end{aligned}$$

Lead Emissions (lb/hr): *Not Applicable*

$$\frac{8.9 \text{ lb/10}^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr}}{1.65 \times 10^{-2} \text{ lb/hr}}$$

26A
 Table A-2:

H₂SO₄ Mist Emissions (lb/hr):

$$\begin{aligned}
 & \text{Based on 8 percent of sulfur converted to acid mist} \\
 & (1,103,099 \text{ cf/hr} \times \frac{1.09 \text{ gr}}{100 \text{ cf}} \times \frac{216 \text{ SO}_2}{16 \text{ S}} \times \frac{1.0 \text{ lb}}{7000 \text{ gr}}) \quad 0.08 \\
 & \frac{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times \frac{3.06 \text{ lb H}_2\text{SO}_4}{\text{lb SO}_2} \times 0.05}{1.53} \\
 & \quad \text{(converted)} \\
 & \quad 0.406 \\
 & - 12.2 \text{ lb/hr}
 \end{aligned}$$

A-26A A-27A A-28A
 Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

$$\begin{aligned}
 & \frac{1,849.9 \text{ (MMBtu)} \times 14 \text{ lb/10}^{12} \text{ Btu}}{2.59 \times 10^{-2} \text{ lb/hr}} \quad \text{Not Applicable}
 \end{aligned}$$

7/31/92

Emission Calculations, Tables A-26A, A-27A, A-28A

Manufacturer/Model: West. 501F
 Fuel Type: Natural Gas
 Load: 70%
 Ambient Temperature: 97°F

Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu = NA lb/hr

Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 1047.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = 1.16 × 10⁻³ lb/hr

Formaldehyde: 88.12 lb/10¹² Btu x 1047.9 MMBtu/hr + 10⁶ MMBtu/10¹² Btu = 9.24 × 10⁻² lb/hr

Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr

Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ = NA lb/hr

Duct Burner - Supplemental Firing
 Natural Gas
 Base Load
 All Temperatures

12018C2/APPA-1
~~06/13/92~~
 7/31/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT
 EXAMPLE CALCULATIONS - ~~27°F~~ ^{All Temperatures given} CONDITIONS
 (From Table A-~~2~~ ¹¹ On ~~Distillate Oil~~; ^{Natural Gas} Base Load)

All Other Calculations on Spreadsheet are Identical.)

¹¹
 Table A-~~4~~ (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10⁶ Btu/hr): 100 mMBtu/hr (given)

~~Power (kW) x Heat Rate (10⁶ Btu/kWh)~~

~~183,700 x 10,070/10⁶ = 1,849.9 x 10⁶ Btu/hr~~

Natural Gas

~~Fuel Oil~~ (lb/hr):

Heat Input (10⁶ Btu/hr) + Fuel Heat Content (Btu/lb)

~~1,849.9~~ x 10⁶ + ~~18,550~~ = ~~99,723~~ lb/hr
 100.0 23,839 4,194.8

Volume Flow (acfm) - See Note A:

V = mRT/PM

~~3,743,000~~ lb/hr x 1,545 x (~~1,060~~²⁰⁵°F + 460°F) + (~~28.25~~^{28.00} x 2,116.8 lb/ft²)
 + 60(min/hr)
~~1,575~~
 = ~~2,456,287~~ acfm

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

68°F
~~3,743,000~~ lb/hr x 1,545 x (68°F + 460°F) + (~~28.25~~^{28.00} x 2,116.8) + 60
~~1,203~~
 = ~~851,152~~ scfm

Duct Burner - Supplemental Firing
 Natural Gas
 Base Load
 All temperatures

12018G2/APPA-
 06/13/92
 7/31/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{1,515}{2,450,287} \text{ acfm} \times (205^\circ\text{F} + 460^\circ\text{F}) + \frac{205}{(1,060^\circ\text{F} + 460^\circ\text{F})}$$

$$- \frac{1,515}{1,072,001} \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\frac{1,515}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$- \frac{0.1}{70.2} \text{ ft/sec}$$

12

Table A-2:

PM emissions in tons per year

$$0.01 \text{ lb/MMBtu} \times 100 \text{ MMBtu/hr} \times 8760 \text{ hr/yr}$$

$$\frac{17 \text{ lb/yr}}{2,000 \text{ lb/ton}} + 2,000 \text{ lb/ton}$$

$$4.38$$

$$- 2.6 \text{ ton/yr}$$

Gas

SO₂ Emissions - ~~oil~~ (lb/hr)

$$\frac{105,263 \text{ cf/hr}}{99,722.19 \text{ lb/hr}} \times \frac{1.0 \text{ gr/100cf}}{0.0005 \text{ lb S/lb}} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb/7000gr}$$

$$0.30$$

$$- 99.72 \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$42 \text{ ppm} \times (20.9 \times (1 - 11.59/100) - 10.96) \times 2,116.8 \text{ lb/ft}^2$$

$$\times \frac{2,450,287 \text{ ft}^3/\text{min}}{60}$$

$$\times 46 \text{ (molecular wt NO}_2\text{)} \times 60 \text{ min/hr} \times [1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F})$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}]$$

$$- 326.2 \text{ lb/hr}$$

$$0.10 \text{ lb/MMBtu} \times 100.0 \text{ MMBtu/hr} = 10.0 \text{ lb/hr}$$

Duct burner - Supplemental Filing
 Natural Gas
 Base Load
 All temperatures

12018C2/APPA-3
 06/12/92
 7/31/92

CO Emissions (lb/hr) - See Note C:

~~30 ppm x (1 - 11.59/100) x 2,450,287 acfm x 2,116.8 lb/ft³ x 28~~
 (molecular wgt. of carbon)

~~x 60 min/hr x (1,543 x (1,060 F + 460 F) x 10⁶)~~

~~98.4 lb/hr~~

0.10 lb/MMBtu x 100.0 MMBtu/hr = 10 lb/hr

VOC Emissions (lb/hr) - See Note C:

~~3.5 ppm x (1 - 11.59/100) x 2,450,287 acfm x 2,116.8 lb/ft³ x 16~~
 (molecular wgt. of methane)

~~x 60 min/hr x (1,543 x (1,060 F + 460 F) x 10⁶)~~

~~6.56 lb/hr~~

0.029 lb/MMBtu x 100.0 MMBtu/hr = 2.90 lb/hr

Lead Emissions (lb/hr): Not Applicable

~~8.9 lb/10¹² Btu x 1,849.9 x 10⁶ Btu/hr = 1.63 x 10⁻² lb/hr~~

¹³
 Table A-3:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

105,263 cf/hr x 100 gr/100 cf x 21 lb SO₂/lb S x 1.0 lb/7000 gr 0.08
~~00,722.0 lb/hr x 0.0005 lb S/lb x 3.06 lb H₂SO₄/lb SO₂ x 0.05~~
 (converted) 1.53
 3.68 x 10⁻²
 = 12.2 lb/hr

A-13, A-14
 Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

~~1,849.9 (MMBtu) x 14 lb/10¹² Btu~~ Not Applicable
 = 2.59 x 10⁻² lb/hr

Emission Calculations, Tables A-13, A-14

Manufacturer/Model: Duct Burner
 Fuel Type: Natural Gas
 Load: 100%
 Ambient Temperature: All Temperatures

- Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr
- Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
- Polycyclic Organic Matter: 1.113 lb/10¹² Btu x 100.0 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = 1.11 × 10⁻⁴ lb/hr
- Formaldehyde: 88.12 lb/10¹² Btu x 100.0 MMBtu/hr + 10⁶ MMBtu/10¹² Btu - 8.81 × 10⁻³ lb/hr
- Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr
- Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr
- Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr
- Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
 = NA lb/hr
- Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ - NA lb/hr

Duct Burner-Supplemented Firing
 Natural Gas
 70% Load
 All Temperatures

12018C2/APPA-1
 06/13/92
 7/31/92

DESTEC CENTRAL FLORIDA COGENERATION PROJECT
 EXAMPLE CALCULATIONS - ~~77°F~~ ^{All Temperatures} CONDITIONS

(From Table A-~~2~~ ^{IIA} On ~~Distillate Oil~~; ^{Natural Gas} 70% LOAD)

All Other Calculations on Spreadsheet are Identical.)

IIA
 Table A-~~2~~: (Note: all other data not calculated but supplied by Manufacturer)

Heat Input (10^6 Btu/hr): 100.0 mmbtu/hr (given)

~~Power (kW) = Heat Rate (10^6 Btu/kWh)~~

~~$183,700 \times 10,070/10^6 = 1,849.9 \times 10^6$ Btu/hr~~

Natural Gas

~~Fuel Oil (lb/hr):~~

Heat Input (10^6 Btu/hr) + Fuel Heat Content (Btu/lb)

$100.0 \quad 23839 \quad 4194.8$
 ~~$1,849.9 \times 10^6 + 18,550 = 96,723$ lb/hr~~

Volume Flow (acfm) - See Note A:

$V = mRT/PM$

$3,743,000 \text{ lb/hr} \times 1,545 \times \frac{5,244}{200} \times (1,060^\circ\text{F} + 460^\circ\text{F}) + \frac{28.00}{20.25} \times 2,116.8 \text{ lb/ft}^2$
 $+ 60(\text{min/hr})$
 ~~$2,450,287$ acfm~~
 $1,504$

Volume Flow (scfm) - See Note A:

Same as volume flow (acfm) except adjusted for standard temperature of

68°F
 $3,743,000 \text{ lb/hr} \times 1,545 \times \frac{5,244}{200} \times (68^\circ\text{F} + 460^\circ\text{F}) + \frac{28.00}{20.25} \times 2,116.8 + 60$
 $1,203$
 ~~$851,152$ scfm~~

Duct Burner - Supplemental Firing
 Natural Gas
 70% LOAD
 All Temperatures

12018G2/APPA-2
 06/13/92
 7/31/92

Volume Flow from HRSG (acfm):

CT Exhaust adjusted for temperature

$$\frac{1,504}{2,450,287} \text{ acfm} \times \frac{200}{(205^\circ\text{F} + 460^\circ\text{F})} + \frac{300}{(1,060^\circ\text{F} + 460^\circ\text{F})}$$

$$= \frac{1,504}{1,072,001} \text{ acfm}$$

Velocity (ft/sec):

Volume Flow (ft³/min) + Area (ft²) + 60 sec/min

$$\frac{1,504}{1,072,001} \text{ ft}^3/\text{min} + 60 + (18.0^2 + 4 \times 3.14159)$$

$$= \frac{0.1}{70.2} \text{ ft/sec}$$

12A
 Table A-2:

PM emissions in tons per year

$$\frac{0.01 \text{ lb/mmBtu} \times 100.0 \text{ mmBtu/hr} \times 8760 \text{ hr/yr}}{2,000 \text{ lb/ton}} \div 2000 \text{ lb/ton}$$

$$= \frac{4.38}{2.6} \text{ ton/yr}$$

SO₂ Emissions--Oil (lb/hr)

$$\frac{105,263 \text{ cc/hr} \times 1.09 \text{ g/100cc}}{99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 2 \text{ lb SO}_2/\text{lb S} \times 1.0 \text{ lb/7000gr}}$$

$$= \frac{0.30}{99.72} \text{ lb/hr}$$

NO_x Emissions (lb/hr) - See Note B:

$$\frac{42 \text{ ppm} \times [20.9 \times (1 - 11.59/100) - 10.96] \times 2,118.8 \text{ lb/ft}^2}{2,450,287 \text{ ft}^3/\text{min}}$$

$$\times 46 \text{ (molecular wgt NO}_2\text{)} \times 60 \text{ min/hr} \times [1,545 \times (1,060^\circ\text{F} + 460^\circ\text{F})]$$

$$\times 5.9 \times 10^6 \text{ (adjust for ppm)}$$

$$= 326.2 \text{ lb/hr}$$

$$0.1 \text{ lb/mmBtu} \times 100.0 \text{ mmBtu/hr} = 10.0 \text{ lb/hr}$$

Duct Burner - Supplemental Firing
Natural Gas
70% Load
All Temperatures

12018C2/APPA-3
06/12/92
7/31/92

CO Emissions (lb/hr) - See Note C:

~~$30 \text{ ppm} \times (1 - 11.59/100) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^3 \times 28$
(molecular wgt. of carbon)~~

~~$\times 60 \text{ min/hr} \times (1,545 \times (1,060^\circ\text{F} - 460^\circ\text{F}) \times 10^6)$~~

~~98.4 lb/hr~~

$0.10 \text{ lb/MMBtu} \times 100.0 \text{ MMBtu/hr} = 10.0 \text{ lb/hr}$

VOC Emissions (lb/hr) - See Note C:

~~$3.5 \text{ ppm} \times (1 - 11.59/100) \times 2,450,287 \text{ acfm} \times 2,116.8 \text{ lb/ft}^3 \times 16$
(molecular wgt. of methane)~~

~~$\times 60 \text{ min/hr} \times (1,545 \times (1,060^\circ\text{F} - 460^\circ\text{F}) \times 10^6)$~~

~~6.56 lb/hr~~

$0.029 \text{ lb/MMBtu} \times 100.0 \text{ MMBtu/hr} = 2.90 \text{ lb/hr}$

Lead Emissions (lb/hr):

Not Applicable

~~$8.9 \text{ lb}/10^{12} \text{ Btu} \times 1,849.9 \times 10^6 \text{ Btu/hr} = 1.65 \times 10^{-2} \text{ lb/hr}$~~

13A

Table A-4:

H₂SO₄ Mist Emissions (lb/hr):

Based on 8 percent of sulfur converted to acid mist

$105,263 \text{ cf/hr} \times 1.0 \text{ gr}/100 \text{ cf} \times 216 \text{ SO}_2 / 165 \times 1.016 / 7000 \text{ gr}$
 ~~$99,722.9 \text{ lb/hr} \times 0.0005 \text{ lb S/lb} \times 3.06 \text{ lb H}_2\text{SO}_4 / \text{lb SO}_2 \times 0.08$~~
(converted) 1.53
 3.68×10^{-2}
 ~~$= 12.2 \text{ lb/hr}$~~

A-13A, A-14A

Tables A-4 and A-5:

EPA emission factor as noted in printout; example for manganese:

~~$1,849.9 \text{ (MMBtu)} \times 14 \text{ lb}/10^{12} \text{ Btu}$~~ Not Applicable

~~$2.59 \times 10^{-2} \text{ lb/hr}$~~

7/31/92

Emission Calculations, Tables A-13A, A-14A

Manufacturer/Model: Duct Burner
Fuel Type: Natural Gas
Load: 70%
Ambient Temperature: All temperatures

Arsenic: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
Beryllium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
Mercury: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr
Fluoride: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Nickel: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Cadmium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Chromium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Copper: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Vanadium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Selenium: _____ lb/10¹² Btu x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu - NA lb/hr

Polycyclic Organic Matter: 1.13 lb/10¹² Btu x 100.0 MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= 1.11 x 10⁻⁴ lb/hr

Formaldehyde: 88.12 lb/10¹² Btu x 100.0 MMBtu/hr + 10⁶ MMBtu/10¹² Btu = 8.81 x 10⁻³ lb/hr

Antimony: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Barium: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Cobalt: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Zinc: _____ pg/J x 2.324 lb/10¹² Btu/pg/J x _____ MMBtu/hr + 10⁶ MMBtu/10¹² Btu
= NA lb/hr

Chlorine: _____ ppm x _____ lb/hr fuel oil + 10⁶ - NA lb/hr

NOTE A

Volume is calculated based on ideal gas law:

$$PV = mRT/M$$

where: P - pressure = 2116.8 lb/ft²
 m - mass flow of gas (lb/hr)
 R - universal gas constant = 1545
 M - molecular weight of gas
 T - temperature (°R)

NOTE B

NO_x is calculated by correcting to 15% O₂ dry conditions using ideal gas law and moisture and O₂ conditions.

Oxygen correction:

$$V_{NOx (15\%)} = \frac{V_{NOx Dry} * 5.9}{20.9 - \%O_2 Dry}$$

(From 40 CFR Part 60; Appendix A, Method 20, Equation 20-4)

$$V_{NOx Dry} = V_{NOx (15\%)} (20.9 - \%O_2 Dry) / 5.9$$

$$\%O_2 Dry = \%O_2 Act / (1 - \%H_2O) ; \%O_2 Act = \%O_2 Dry (1 - \%H_2O)$$

(From Method 20; Equation 20-1)

$$V_{NOx Act} = V_{NOx Dry} (1 - \%H_2O); (From Method 20; Equation 20-1)$$

Substituting:

$$\begin{aligned} V_{NOx Act} &= V_{NOx 15\%} (20.9 - \%O_2 Dry) (1 - \%H_2O) / 5.9 \\ &= V_{NOx (15\%)} [20.9 - (\%O_2 Act / (1 - \%H_2O))] (1 - \%H_2O) / 5.9 \\ &= V_{NOx (15\%)} [20.9 (1 - \%H_2O) - \%O_2] / 5.9 \end{aligned}$$

$$m_{NOx} = \frac{PVM_{NOx}}{RT} = \frac{V_{NOx (15\%)} [20.9 (1 - \%H_2O) - \%O_2] * P * M_{NOx}}{RT * 5.9}$$

NOTE C

Same as D except only moisture correction is used:

$$V_{CO \text{ Act}} - V_{CO \text{ Dry}} (1 - \%H_2O)$$

$$m_{CO} - PV_{CO \text{ Act}} M_{CO} / RT$$

$$- PV_{CO \text{ Dry}} (1 - \%H_2O) M_{CO} / RT$$



UNITED STATES ENVIRONMENTAL PROTECTION AGENCY

REGION IV

345 COURTLAND STREET, N.E.
ATLANTA, GEORGIA 30365

4APT-AEB

JUL 15 1992

RECEIVED

JUL 20 1992

Bureau of
Air Regulation

Mr. Clair H. Fancy, P.E., Chief
Bureau of Air Regulation
Florida Department of Environmental
Regulation
Twin Towers Office Building
2600 Blair Stone Road
Tallahassee, Florida 32399-2400

RE: Central Florida Power Limited Partnership,
Central Florida Cogeneration Plant (PSD-FL-190)

Dear Mr. Fancy:

This is to acknowledge receipt of the Prevention of Significant Deterioration (PSD) permit application package for the above referenced facility. The proposed facility will be a combined cycle cogeneration power plant, nominally rated at 206 megawatts for the facility. The proposed project consists of one advanced technology heavy-duty industrial gas turbine electric generating unit, with a duct burner-fired heat recovery steam generator, and a steam turbine generator.

The applicant proposes to limit NO_x emissions from the combustion turbine through advanced dry low-NO_x combustors and water injection, to limit NO_x emissions from the duct burner through combustion design, to limit CO emissions from the combustion turbine and duct burner through combustion design, and to limit VOC, PM/PM₁₀, Be, and As emissions from the combustion turbine through combustion control and the use of clean fuels.

We have reviewed the package as submitted and have no adverse comments. Thank you for the opportunity to review and comment on the package. If you have any questions or comments, please contact Mr. Scott Davis of my staff at (404) 347-5014.

Sincerely yours,

Jewel A. Harper, Chief
Air Enforcement Branch
Air, Pesticides, and Toxics
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