Golder Associates Inc.

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December 15, 2005

BUREAU OF AIR REGULATION

053-7537

Florida Department of Environmental Protection 2600 Blair Stone Road, MS #5505 Tallahassee, FL 32399-2400

Attention: Mr. Jeffery Koerner, Air Permitting North

RE: OKEELANTA CORPORATION/NEW HOPE POWER PARTNERSHIP
PROJECT NOS. 0990005-016-AC AND 0990005-017-AV
TITLE V PERMIT RENEWAL AND CONCURRENT AIR CONSTRUCTION PERMIT
REVISION

Dear Mr. Koerner:

Okeelanta Corporation and New Hope Power Partnership (NHPP) have received the Department's request for additional information (RAI) dated June 30, 2005, regarding the Title V renewal application. Each of the Department's requests is answered below, in the same order as they appear in the RAI letter.

1. Attachment OC-FI-CV6: This attachment requests several changes to permit conditions that were previously requested, but not granted. For each requested change, provide the current permit condition, the revised permit condition, and the underlying air construction permit or regulatory citation. The Department will consider your requests, but must determine the possible implications from making such changes (i.e., affects on a BACT determination, PSD avoidance, etc.). After this information is provided, I recommend a meeting to resolve the requested changes.

Response: The Department requests that Attachment OC-FI-CV6 be revised to identify the current permit condition, the revised permit condition, and the underlying air construction permit. Attached is a revised Attachment OC-FI-CV6, with additional information added. Golder will also be submitting in the near future an electronic markup of the draft Title V permit, with the suggested wording. The electronic markup also will contain reference to the underlying air construction permit associated with each requested change. We would be glad to meet with you to discuss these requested changes.

- 2. <u>Attachment OC-FI-CV3a Compliance Plan</u>: This attachment identifies potential compliance issues and a plan to regain compliance.
 - a. Boiler 16: What is the current operational status for this unit? Describe the operational scenarios during which this boiler is operated, the frequency, and duration. What is the current fuel sulfur content? Was an initial certification of the NO_x CEMS ever performed and satisfactorily completed?

b. Central Vacuum System (EU-018): What are the problems with this equipment? Why isn't this equipment being used?

Response:

a. Boiler No. 16 currently operates infrequently as a backup to the cogeneration boilers. During calendar year 2003, Boiler No. 16 operated only 1,224 hours. During 2004, the boiler operated only 20 hours for the sole purpose of conducting a RATA for the nitrogen oxides (NO_x) continuous emissions monitoring system (CEMS). The boiler has not operated in 2005. The boiler has burned natural gas during the most recent operation, but could burn up to 0.05 percent sulfur fuel oil under its air permit. An initial CEMS certification was performed on the boiler in 2004, except for the 7-day drift test.

Okeelanta is proposing to reduce the permitted annual capacity factor for Boiler No. 16 to 10 percent or less. This will eliminate the NO_x emission limit and the requirement for a CEMS for NO_x under Subpart Db. The requirement for a continuous opacity monitoring system (COMS) will remain, but Okeelanta is requesting an Alternative Monitoring Plan consisting of daily visible emissions observations, as has been approved for other similar Subpart Db boilers. An air construction permit application incorporating this change has recently been submitted under separate cover.

b. The main problem with this equipment is that the ductwork from the vacuum points to the control device plugs up with sugar dust. The ductwork needs to be thoroughly cleaned or replaced. Okeelanta may upgrade the ductwork in the future to reduce this problem. At present, Okeelanta is not using this equipment.

3. CAM Plan

- a. Cogeneration Boilers A, B, and C: The indicator for particulate matter is opacity and you have proposed 20% based on a 1-hour block average. Identify other critical parameters for the electrostatic precipitator that may also be included in the CAM plan to ensure continuous compliance with the particulate matter standard.
- b. Central Dust Collection System Nos. 1 and 2 (EU-021 and 022) and Cooler No. 2 (EU-024): Explain the problems with "fouling" of the instrument sample line for monitoring the pressure drop across the wet cyclone. What corrective actions could be taken to prevent fouling?

Response:

a. In the proposed CAM Plan (May 18, 2005), NHPP submitted opacity data collected during the annual emission compliance tests that establishes a correlation between opacity and particulate matter (PM) emissions (see Figure C-1 in CAM Plan). Based upon this correlation, NHPP believes that opacity is the surrogate that would most accurately reflect compliance with the PM standard. NHPP's operating experience has shown that ESP parameters (i.e., secondary voltage and current, or total secondary power) vary widely and probably would not correlate well as a compliance indicator for PM emissions. This is due to the non-homogeneous characteristics of bagasse and wood fuel fired at the facility. These fuel characteristics include high and low ash content, high and low moisture content, high resistivity versus low resistivity, etc. Therefore, we do not believe there are any ESP parameters which could be reliably included in the CAM Plan.

b. Sugar dust coupled with a very moist environment results in fouling and plugging of small openings. The moist sugar dust, after passing through the wet cyclones, is hygroscopic and very sticky. The small openings of the pressure indicator sample lines therefore plug rapidly. The only way to prevent this would be to implement a highly intensive maintenance program, which would be costly. Also, we believe that since the wet rotoclones are passive devices, the water flow rates to the rotoclones are the primary indicator of PM removal efficiency. For these reasons, it is requested that only water flow rate be the indicator parameter for the CAM Plan.

Note that the wet cyclones have now been replaced by wet rotoclones, as authorized by the Department's letter dated November 16, 2004. The facility plot plan (Attachment OC-FI-C1) has been updated to reflect this, as well as the sugar refinery emissions unit section, and are attached. Also, an updated CAM plan that reflects these revised emissions units is attached. Since visible emissions tests have not yet been conducted on the Wet Rotoclones Nos. 3 and 4, minimum water flow rate values cannot be set. However, these tests will be conducted in the near future and the water flow rates recorded to set the minimum parameter values. The Department may elect to add this item to the compliance plan for Okeelanta, i.e., the requirement and schedule to perform the VE testing and parameter value monitoring for Wet Rotoclones Nos. 3 and 4.

Thank you for consideration of this information. If you have any questions, please do not hesitate to call me at (352)336-5600.

Sincerely,

GOLDER ASSOCIATES INC.

David a. Suff

David A. Buff, P.E., Q.E.P.

Principal Engineer

Enclosures

DB/all

cc:

Bill Tarr Matt Capone James Meriwether David Dee

Jose Garcia, PBCHD

Ron Blackburn, FDEP Ft. Myers

0537537/4.1/RAI L121505.doc

APPLICATION INFORMATION

Profess	sional Engineer Certification
1. Pro	fessional Engineer Name: David A. Buff
	Registration Number: 19011
2. Pro	fessional Engineer Mailing Address
1	ganization/Firm: Golder Associates Inc.**
	Street Address: 6241 NW 23 rd Street, Suite 500
	City: Gainesville State: FL Zip Code: 32653
3. Pro	fessional Engineer Telephone Numbers
Tel	ephone: (352) 336-5600 ext.545 Fax: (352) 336-6603
	fessional Engineer Email Address: dbuff@golder.com
5. Pro	fessional Engineer Statement:
I, th	ne undersigned, hereby certify, except as particularly noted herein*, that:
unit prop poll	To the best of my knowledge, there is reasonable assurance that the air pollutant emissions t(s) and the air pollution control equipment described in this application for air permit, when perly operated and maintained, will comply with all applicable standards for control of air lutant emissions found in the Florida Statutes and rules of the Department of Environmental tection; and
are calc emi	To the best of my knowledge, any emission estimates reported or relied on in this application true, accurate, and complete and are either based upon reasonable techniques available for culating emissions or, for emission estimates of hazardous air pollutants not regulated for an ssions unit addressed in this application, based solely upon the materials, information and culations submitted with this application.
so), prop app	If the purpose of this application is to obtain a Title V air operation permit (check here , if I further certify that each emissions unit described in this application for air permit, when perly operated and maintained, will comply with the applicable requirements identified in this lication to which the unit is subject, except those emissions units for which a compliance plan schedule is submitted with this application.
cond revi so), app four	If the purpose of this application is to obtain an air construction permit (check here \square , if so) or currently process and obtain an air construction permit and a Title V air operation permit is ion or renewal for one or more proposed new or modified emissions units (check here \square , if I further certify that the engineering features of each such emissions unit described in this lication have been designed or examined by me or individuals under my direct supervision and and to be in conformity with sound engineering principles applicable to the control of emissions the air pollutants characterized in this application.
revi if so eaci info	If the purpose of this application is to obtain an initial air operation permit or operation permit is ion or renewal for one or more newly constructed or modified emissions units (check here), I further certify that, with the exception of any changes detailed as part of this application, h such emissions unit has been constructed or modified in substantial accordance with the symmetry, given in the corresponding application for air construction permit and with all
pro	visions contained in such permit.
	12/15/05 12/15/05
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* A	ach any exception to certification statement.

DEP Form No. 62-210.900(1) – Form Effective: 06/16/03

APPLICATION INFORMATION

Application Responsible Official Certification

Complete if applying for an initial/revised/renewal Title V permit or concurrent processing of an air construction permit and a revised/renewal Title V permit. If there are multiple responsible officials, the "application responsible official" need not be the "primary responsible official."

_	11 1 2 2 1 1 2 2 2 1 1 2 2										
1.	Application Responsible Official Name: Ricardo A. Lima, Vice President and General Manager										
2.	Application Responsible Official Qualification (Check one or more of the following options, as applicable):										
	For a corporation, the president, secretary, treasurer, or vice-president of the corporation in charge of a principal business function, or any other person who performs similar policy or decision-making functions for the corporation, or a duly authorized representative of such person if the representative is responsible for the overall operation of one or more manufacturing, production, or operating facilities applying for or subject to a permit under Chapter 62-213, F.A.C.										
	For a partnership or sole proprietorship, a general partner or the proprietor, respectively.										
	For a municipality, county, state, federal, or other public agency, either a principal executive										
	officer or ranking elected official.										
	☐ The designated representative at an Acid Rain source.										
3.	Application Responsible Official Mailing Address										
	Organization/Firm: Okeelanta Corporation										
	Street Address: 21250 U.S. Highway 27 South										
	City: South Bay State: FL Zip Code: 33493										
4.	Application Responsible Official Telephone Numbers Telephone: (561) 993-1600 ext. Fax: (561) 992-7326										
5.	Application Responsible Official Email Address:										
6.	Application Responsible Official Certification:										
	I, the undersigned, am a responsible official of the Title V source addressed in this air permit application. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements made in this application are true, accurate and complete and that, to the best of my knowledge, any estimates of emissions reported in this application are based upon reasonable techniques for calculating emissions. The air pollutant emissions units and air pollution control equipment described in this application will be operated and maintained so as to comply with all applicable standards for control of air pollutant emissions found in the statutes of the State of Florida and rules of the Department of Environmental Protection and revisions thereof and all other applicable requirements identified in this application to which the Title V source is subject. I understand that a permit, if granted by the department, cannot be transferred without authorization from the department, and I will promptly notify the department upon sale or legal transfer of the facility or any permitted emissions unit. Finally, I certify that the facility and each emissions unit are in compliance with all applicable requirements to which they are subject, except as identified in compliance plan(s) submitted with this application.										
	Signature Date										

DEP Form No. 62-210.900(1) – Form Effective: 06/16/03

ATTACHMENT OC-FI-CV6

REQUESTED CHANGES TO CURRENT TITLE V OPERATION PERMIT

(revised 12-15-2005)

The current Title V Permit No. 0990005-012-AV for Okeelanta Corporation was issued on March 18, 2004, by the Florida Department of Environmental Protection (FDEP). The permit covers the Okeelanta Corporation (Okeelanta) facilities, including the Okeelanta sugar mill, refinery, and trans-shipment facilities, and the New Hope Power Partnership (NHPP) cogeneration facility. After a draft of the permit was issued on September 12, 2003, Mr. Ricardo Lima of Okeelanta requested some minor changes and clarifications to the permit in a letter to the FDEP dated October 24, 2003. However, a number of these changes were not incorporated into the final permit.

The same changes were also requested in the Title V permit revision application that was submitted to the FDEP in April 2004 for a revision to Boilers A, B, and C, and the material handling and storage operation of the NHPP cogeneration facility. Since a revised Title V permit has not been issued since April 2004, this renewal application for the Title V permit for Okeelanta also requests the same corrections, minor changes and clarifications that have been revised to reflect the most recent changes to the facility.

The following major changes are reflected in this Title V renewal application:

- Revision of the NHPP cogeneration boilers' heat input rates.
- Revision of New Source Performance Standards (NSPS) storage tanks from regulated to unregulated emissions units since they no longer are subject to Subpart Kb. Subpart Kb was revised on October 15, 2003. The tanks are between 75 and 151 cubic meters (m³) in size and store volatile organic liquid with a vapor pressure less than 15.0 kiloPascals (kPa).
- Reduction of mercury test frequency for the NHPP cogeneration boilers.
- Incorporation of modifications to the paint spray booth as reflected in air construction permit no. 0990005-015-AC dated November 2, 2005. Updated pages to the paint booth emissions unit section are attached to support this request. It is requested that the revisions to the construction permit be reflected in the renewed Title V permit.
- Incorporation of modifications to the sugar refinery emissions unit reflecting the newly installed wet rotoclones Nos. 3 and 4 that replaced the wet cyclones Nos. 1 and 2, per the

letter of authorization from the FDEP dated November 16, 2004. Updated pages to the sugar refinery emissions unit section and CAM Plan are attached to support this request. It is requested that these revisions be reflected in the renewed Title V permit.

Also included is a revised "Wood, Bagasse, and Ash Inspection and Testing Plan" (Attachment OC-EU5-I5) and an operating procedure (Attachment OC-EU5-ARC) that addresses inclement weather operations for the NHPP cogeneration facility.

The minor changes and clarifications to the existing Title V Permit No. 0990005-012-AV, originally requested in the letter from Mr. Ricardo Lima, Okeelanta, dated October 24, 2003, are presented below:

Referenced attachments made a part of this permit:

Page 2 Comment. Add Appendix CP-1, Compliance Plan, in accordance with Facility-Wide Condition 12.

SECTION I. Facility Information

Subsection A.

Facility Description

Page 3. New Comment. Deleted "Kb" from fifth paragraph listing of applicable 40 CFR 60 Subparts.

Subsection B.

EU ID Nos. & Brief Description

Page 4. New Comment. Change status of the emissions unit (EU) ID Nos. 015, 016, and 017 to Unregulated.

Page 4. Comment I.B.(4). In a letter submitted to the FDEP on March 28, 2003, Okeelanta requested that the permit be revised to change the three sugar silos (EUs 026, 027, and 028) to a single emissions unit with three exhaust points. Since the silos were designed and have always operated as a single automated system, revising the permit in this manner is a more accurate description of the source. It is suggested that the brief description list be revised as follows:

EU ID No.	Status	Brief Description
026	Regulated	Sugar silos (S1101, S1102, and S1103)
027	N/A	Re-designated as part of EU 026
028	N/A	Re-designated as part of EU 026

Page 4. Comment I.B.(2). EU ID No. 045 Brief Description:

Replace "Main Sugar Receiver" with "Powdered Sugar Dryer/Cooler Baghouse."

Page 4. Comment I.B.(3). EU ID Nos. 045, 046, and 047 should be listed as "Regulated."

Subsection C. Relevant Documents

Page 6. Comment I.C. Restate EU 045 as "Powdered Sugar Dryer/Cooler Baghouse (EU 045)" for listing permit document "0990005-013-AC, Construction Permit."

Page 6. New Comment. Add Construction Permit No. 0990005-015-AC to list for EU 048

SECTION II. Facility-wide Conditions

Page 7. Comment II.4. Re-insert wording "when applicable" at the end of paragraph 4(a).

SECTION III. Emissions Units and Conditions

Subsection A. Mill Boiler No. 16

Continuous Monitoring Requirements

Page 16. Condition A.10.d. In paragraph "d," reference to Condition No. 11 should be changed to Condition No. A.7.

Page 17. Condition A.12. In the second sentence, replace "in Appendix XS" with "by Condition A.15."

Recordkeeping and Reporting Requirements

Page 18. Condition A.15. In the third sentence, replace "Appendix XS of this permit" with "40 CFR 60.7 and Figure 1 attached to this permit."

Subsection B. NSPS Storage Tanks

Pages 19-20. Okeelanta requests that these EUs be deleted and the storage tanks listed as unregulated EUs. The tanks are between 75 and 151 m³ in size and store volatile organic liquids

with a vapor pressure less than 15.0 kPa, which makes them exempt from Subpart Kb, per the recent revision that took effect on October 15, 2003. The previous comments, submitted prior to this subsection becoming obsolete, are listed below.

Emissions Unit Details

Page 19. Condition B.2. Change two references of EU ID No. 033 to 005.

Compliance Demonstrations and Periodic Monitoring

Page 20. Condition B.5. Change reference of Condition E.4. to Condition B.4.

Page 20. Condition B.6.b. Change paragraph (b) to delete reference to monitoring and recording of true vapor pressure. This is consistent with Section 2 of the Compliance Plan (Appendix CP-1) made part of this permit by Condition II.12.

Subsection C. Trans-shipment Facility

Page 21. <u>Brief Description</u>. Okeelanta requests that EU 026 be described as "Sugar Silos (S1101, S1102, and S1103)," and that references to EUs 027 and 028 be deleted. Since the sugar-receiving silos were designed and operate as a single system, revising the permit to one emissions unit including the silos and their three emission points is a more accurate description of the source. EUs 045, 046, and 047 should be added to this subsection.

Emissions Unit Details

Page 21. For clarification, it is suggested that the last sentence of the first paragraph be separated from the paragraph and reworded as follows:

"The facility also includes original packaging lines and sugar grinder baghouses, refined sugar-receiving silos, a new powdered sugar dryer/cooler with baghouse, a new sugar grinder with baghouse, and new packaging lines with baghouse."

- Page 21. The last sentence of the second paragraph should be deleted since the new packaging lines (EU 047) have no connection to the existing packaging lines (EU 019).
- Page 21. The last sentence of the third paragraph should be deleted since the new powdered sugar dryer/cooler with baghouse (EU 045) has no connection to the existing sugar grinder and hopper (EU 020).

Page 21. Designate silos S1101, S1102, and S1103 as EU 026, and delete reference to EUs 027 and 028. Add descriptions for EUs 045, 046, and 047.

Construction Restrictions

Page 22. Condition C.1. Please delete this condition since this refers to control equipment specifications that are detailed in the construction application, but have no basis for being permit conditions. If this condition is retained, change both EUs 027 and 028 to 026 in the table. Add descriptions and information for EUs 045, 046, and 047.

Essential Potential to Emit (PTE) Parameters

Page 23. Condition C.2. Change EUs 027 and 028 to 026. Add EU 047 with process capacity of 865 tons/day. Add a note at the bottom of the table to indicate that the daily process capacity of 865 tons/day for EUs 019 and 047 is the combined capacity for all packaging lines. Change note (1) for EU 019 to "Maximum Loading to packaging lines 1 through 9."

Page 23. Condition C.3(b). Change to authorize 9 original packaging lines (EU 019) and in addition four new packaging lines (EU047) to operate simultaneously up to the maximum process rate (865 tons/day) specified in Condition C.2.

Page 23. Condition C.3(c). Change to authorize operation of new sugar grinder and hopper (EU 046) in addition to original grinder and hopper (EU 020).

Page 23. Condition C.3(e). Add to authorize operation of new powdered sugar dryer/cooler (EU 045).

Page 23. Condition C.4. Add references to EUs 045, 046, and 047 in authorization to operate continuously.

Emission Limitations and Standards

Page 24. Condition C.5. Delete reference to EUs 027 and 028, and add EUs 045, 046, and 047.

Page 24. Condition C.6. Change EU 019 limit to 3.754 tons per year (TPY). Change the limit of EU 020 to 0.060 TPY. Add EU 045 (3.379 TPY), EU 046 (0.676 TPY), and EU 047 (2.253 TPY). (See Attachment OC-EU2-F1.8 submitted with Okeelanta's renewal application to revise the permit for calculations of potential annual emissions from each unit.)

Compliance Demonstration and Periodic Monitoring

Page 25. Condition C.11. Okeelanta requests that the words "silo loaded" be deleted from paragraph (d). Okeelanta requests that the Title V permit be revised to allow recording of the total amount of sugar transferred to the three silos on a 24-hour basis. There is no corresponding condition in the underlying construction permit (Permit No. 0990005-008-AC) that would require recording sugar transferred to each individual silo. This is consistent with the Compliance Plan (Appendix CP-1) made part of this permit by Condition II.12.

Subsection D. Sugar Refinery

Brief Description

Page 26. Change wet cyclone No. 1 and No. 2 to wet rotoclone No. 3 and No. 4, respectively, to reflect the recent changes to the facility.

Emissions Unit Details

Page 26. Replace 'wet cyclones" with "wet rotoclones" and number appropriately. Update stack heights.

Page 26. Comment III.D. The last paragraph describing EU 035 states incorrectly that the transfer bulk load-out operation is fed from the other bulk load-out operation (EU 034). The description should state that the 4 enclosed conveyors feed sugar in series from the refinery (curing bins or refined sugar storage silo).

Construction Restrictions

Page 27. Condition D.1. Please delete this condition since this is referring to control equipment specifications that are detailed in the construction application, but have no basis for being permit conditions.

Page 27. Condition D.1(b). If this condition is retained, the cyclonic control devices include specifications for water injection rate and pressure drop. The specifications should be identical to those identified in the permit application dated October, 2004, to replace the refinery wet cyclones. However, the cyclonic control device specifications were either based on stack tests of manufacturer's design data or just manufacturer's design data. Furthermore, measuring the pressure drop continually in these control devices has proven to be impractical due to fouling in the instrument sample lines. Okeelanta has requested that the pressure drop column be deleted

and that only the water injection rate be included in the construction restrictions conditions. The minimum water injection rates should be changed to 2 gallons per minute (gpm) for EUs 021, 022, 023 and 024. This request is consistent with Section 6 of the Compliance Plan (Appendix CP-1) in the Title V permit and the January 2003 conference call with the FDEP and Okeelanta.

Essential Potential to Emit (PTE) Parameters

Page 28. Condition D.2. The process rate capacity table is incorrect. There is no basis in the underlying construction permits to impose an hourly process rate restriction to the refinery sources. Therefore, the table should be modified as shown in the markup.

Page 29. Condition D.6(d). The maximum feed rate authorized for the fluidized bed dryer/cooler should be changed to 1,200 TPD as specified in the permit application. Construction Permit No. 0990005-005-AC, dated January 19, 2001, should be referenced.

Page 29. Condition D.7. The previous limitation on hours of operation is obsolete since Permit No. 0990005-005-AC became effective. The operation is limited instead by the new maximum process rates. All refinery equipment should be authorized to operate continuously within the established production limitations.

Emission Limitations and Standards

Page 30. Condition D.9. Particulate matter emission limitation should be changed to reflect permit No. 0990005-005-AC and the corresponding permit application. The allowable emission table should be changed as shown in the markup.

Subsection E. Material Handling (Cogeneration Facility)

Pages 32-36. Comment E. Various references to coal storage and handling should be deleted.

Subsection F. Cogeneration Boilers

Update this entire section to reflect permit no. PSD-FL-196(O).

Compliance Methods and Reporting

Page 48. Comment F.20.b. Mercury emissions are tested annually based on specific condition III.19.b. of permit no. PSD-FL-196(O). Based on the actual test data presented in the following table, the mercury emissions from the cogeneration boiler range between 2.66E-07 and 3.68E-06 pounds per million British thermal units (lb/MMBtu), well below the mercury

Mercury Emissions

		sting: 02/12/02 chanical Dust			Stack Testing: 01/21/03 - 01/23/03 Post-Mechanical Dust Collectors			sting: 02/11/04 chanical Dust		Stack Testing: 02/22/05 - 02/24/05 Post-Mechanical Dust Collectors			
	Unit A	Unit B	Unit C	Unit A Unit B Unit C Biomass Biomass Biomass			Unit A	Unit B	Unit C	Unit A	Unit B	Unit C	
Pollutant	Biomass (Ib/MMBtu)	Biomass (lb/MMBtu)	Biomass (lb/MMBtu)	Biomass (lb/MMBtu)	Biomass (lb/MMBtu)	Biomass (lb/MMBtu)	Biomass (lb/MMBtu)	Biomass (lb/MMBtu)	Biomass (lb/MMBtu)	Biomass (lb/MMBtu)	Biomass (lb/MMBtu)	Biomass (lb/MMBtu)	
	(RO/TVTTVTDtu)	(10/14/14/Dtu)	(10/1VIIVIDIU)	(lo/iviivibtu)	(ID/IVIIVIDEU)	(ID/TVTTVIDEG)	(ID/IVIIVIDIU)	(IO/IVIIVIDIU)	(ID/IVIIVIBIU)	(10/1VIIVIBILI)	(ID/IVIIVIBILI)	(ID/IVIIVIBLU)	
Particulate (TSP)	0.008	0.010	0.011	0.0089	0.0079	0.0081	0.0068	0.0098	0.0123	0.0162	0.0145	0.0123	
Particulate (PM ₁₀)	0.008	0.010	0.011										
VOCs	0.007	0.036	0.020	0.0027	0.0057	0.058	0.0057	0.0067	0.0063	0.0013	0.0190	0.0063	
Lead	2.08E-05	1.41E-05	2.09E-05										
Mercury	1.65E-06	9.70E-07	3.68E-06	7.55E-07	8.51E-07	1.10E-06	6.24E-07	3.51E-07	6.14E-07	2.66E-07	1.32E-06	6.14E-07	

Sources: Air Consulting Engineering, Inc., 2005; Golder, 2005 Note: Biomass firing consisted of approximately 50% wood and 50% bagasse.

TSP = Total suspended particulate. $PN_{10} = Particulate$ matter less than 10 microns. VOCs = Volatile organic compounds.

emissions limit of 5.4x10⁻⁶ lb/MMBtu. Based on the consistency of actual emissions, which are well below the allowable emissions, it is requested that mercury be removed from the annual testing requirement. Based on Condition F.20, mercury emissions will be tested every 5 years upon permit renewal. In addition, only one of the three boilers should be required to be tested since all the boilers are identical and are burning the same fuel from a common fuel supply.

Subsection G. Paint Booth

Update this entire section to reflect permit no. 0990005-015-AC.

Page 52. Comment G.2. Delete third and fourth sentences of "Methods of Operation" paragraph to allow different manufacturers and models of the airless paint spray system so long as the airless application system is of equivalent or better efficiency.

Subsection H. Common Conditions

EU ID No., Status and Brief Description

Page 56. Comment H(1). The status and description of the retired mill boilers (EUs 003 through 013) should indicate "N/A" and "Shutdown," consistent with Section I.B. (pages 4 and 5).

Page 56. Comment H(2). Okeelanta has requested that EUs 027 and 028 be redesignated as part of EU 026. Please refer to Comment I.B(1) above.

Page 56. Comment H(3). The Transfer Bulk Load-out Operation EU ID No. should be corrected to 035. EUs 045, 046, 047, and 048 should be added to the list.

SECTION IV. ATTACHMENTS

Please include Appendix CP-1, Compliance Plan, made part of the permit by Facility-wide Condition II.12.

Appendix RBL-001 Comment. This appendix should be updated to include the most recent best available control technology (BACT) determinations for EU 014 on October 29, 2001.

Appendix U-1 Comment. The last two sections of unregulated EUs and/or activities in this appendix (Cogeneration Facility and Trans-shipment Facility) should be assigned new ID numbers that are not assigned to other emissions units listed on Page 4 of the permit.

TABLE OF CONTENTS

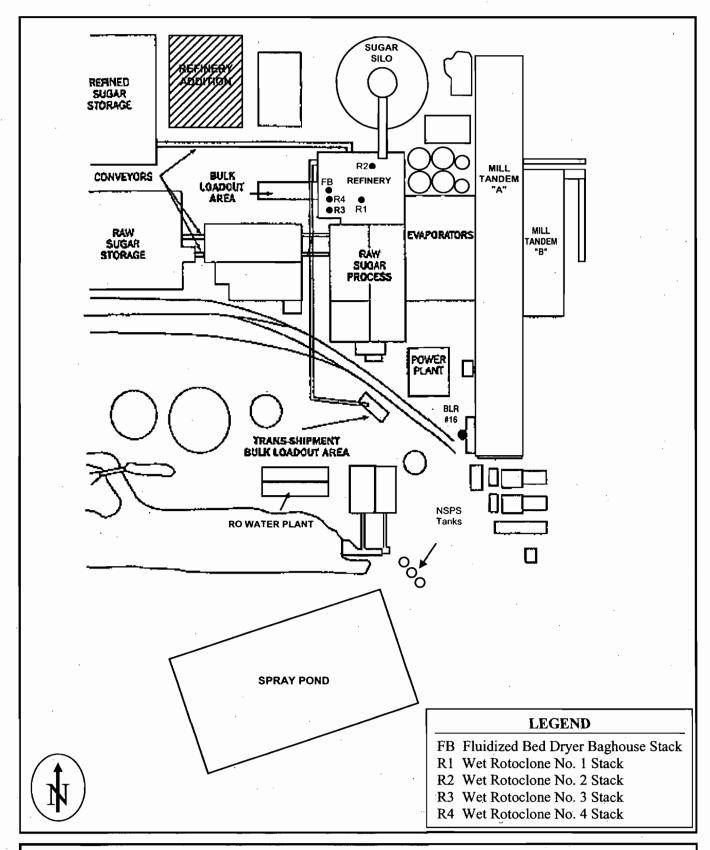
Table of Contents Comment. Suggest referencing Section III.C. as "Trans-shipment Facility" and Section III.D. as "Sugar Refinery." The page number column information needs to be updated. Please list Appendix CP-1, Compliance Plan.

REVISIONS TO TITLE V APPLICATION FORMS

ATTACHMENT OC-FI-C1

FACILITY PLOT PLAN

12/15/05



Attachment OC-FI-C1

Facility Plot Plan of Okeelanta Sugar Mill and Refinery

Note: Plot Plan is a general arrangement for informational purposes only. Plot plan is not to scale



ATTACHMENT OC-FI-CV6

REQUESTED CHANGES TO CURRENT TITLE V OPERATION PERMIT

ATTACHMENT OC-FI-CV6

REQUESTED CHANGES TO CURRENT TITLE V OPERATION PERMIT

(revised 12-15-2005)

The current Title V Permit No. 0990005-012-AV for Okeelanta Corporation was issued on March 18, 2004, by the Florida Department of Environmental Protection (FDEP). The permit covers the Okeelanta Corporation (Okeelanta) facilities, including the Okeelanta sugar mill, refinery, and trans-shipment facilities, and the New Hope Power Partnership (NHPP) cogeneration facility. After a draft of the permit was issued on September 12, 2003, Mr. Ricardo Lima of Okeelanta Corporation requested some minor changes/clarification to the permit in a letter to FDEP, dated October 24, 2003. However, a number of these changes were not incorporated into the final permit.

The same changes were also requested in the Title V permit revision application which was submitted to FDEP in April, 2004 for a revision to Boilers A, B, and C, and the material handling and storage operation of the NHPP cogeneration facility. Since a revised Title V permit has not yet been issued since April 2004, this renewal application for the Title V permit for Okeelanta Corporation also requests the same corrections, minor changes and clarifications, which have been revised to reflect the most recent changes to the facility. The following major changes are reflected in this Title V renewal application:

- Revision of the NHPP cogeneration boilers' heat input rates.
- Revision of NSPS storage tanks from regulated to unregulated emissions units, since they are no longer subject to Subpart Kb. Subpart Kb was revised on October 15, 2003. The tanks are between 75 and 151 cubic meters (m³) in size and store volatile organic liquid with a vapor pressure less than 15.0 kiloPascals (kPa).
- Reduction of mercury test frequency for the NHPP cogeneration boilers.
- Incorporate modifications to the paint spray booth as reflected in the air construction permit no. 0990005-015-AC dated November 2, 2005. Updated pages to the paint booth emissions unit section are attached to support this request. It is requested that the revisions to the construction permit be reflected in the renewed Title V permit.
- Incorporate modifications to the Sugar Refinery emissions unit, reflecting the newly installed wet rotoclones Nos. 3 and 4, which replaced the Wet Cyclones Nos. 1 and 2, per letter authorization from the Department dated November 16, 2004. Updated pages to the

Sugar Refinery emissions unit section and CAM Plan are attached to support this request. It is requested that these revisions be reflected in the renewed Title V permit.

Also included is a revised "Wood, Bagasse, and Ash Inspection and Testing Plan" (Attachment OC-EU5-I5) and an operating procedure (Attachment OC-EU5-ARC) that addresses inclement weather operations for the NHPP cogeneration facility.

The minor change/clarifications to the existing Title V Permit No. 0990005-012-AV, originally requested in a letter from Mr. Ricardo Lima, Okeelanta Corporation, dated October 24, 2003, are presented below:

Referenced attachments made a part of this permit:

Page 2 Comment. Add Appendix CP-1, Compliance Plan in accordance with Facility-Wide Condition 12.

SECTION I. Facility Information

Subsection A.

Facility Description

Page 3. New Comment. Deleted "Kb" from 5th paragraph listing of applicable 40 CFR 60 Subparts.

Subsection B.

EU ID Nos. & Brief Description

Page 4. New Comment. Change status of E.U. ID No.'s 015, 016, & 017 to Unregulated.

Page 4. Comment I.B(4). In a letter submitted to FDEP on March 28, 2003, Okeelanta requested that the permit be revised to change the three sugar silos [Emissions Units (EUs) 026, 027, and 028] to a single emissions unit with three exhaust points. Since the silos were designed and have always operated as a single automated system, revising the permit in this manner is a more accurate description of the source. It is suggested that the brief description list be revised as follows:

EU ID No.	<u>Status</u>	Brief Description
026	Regulated	Sugar Silos (S1101, S1102, and S1103)
027	N/A	Re-designated as part of EU 026

028

Re-designated as part of EU 026

Page 4. Comment I.B.(2). EU ID No. 045 Brief Description:

N/A

Replace "Main Sugar Receiver" with "Powdered Sugar Dryer/Cooler Baghouse".

Page 4. Comment I.B.(3). EU ID Nos. 045, 046, and 047 should be listed as "Regulated".

Subsection C. Relevant Documents

Page 6. Comment I.C. Re-state EU 045 as "Powdered Sugar Dryer/Cooler Baghouse (EU 045)" for listing permit document "0990005-013-AC, Construction Permit".

Page 6. New Comment. Add Construction Permit No. 0990005-015-AC to list for E.U. 048

SECTION II. Facility-wide Conditions

Page 7. Comment II.4. Re-insert wording "when applicable" at the end of paragraph 4(a).

SECTION III. Emissions Units and Conditions

Subsection A. Mill Boiler No. 16

Continuous Monitoring Requirements

Page 16. Condition A.10.d. In paragraph "d", reference to Condition No. 11 should be changed to Condition No. A.7.

Page 17. Condition A.12. In the second sentence, replace "in Appendix XS" with "by Condition A.15."

Recordkeeping and Reporting Requirements

Page 18. Condition A.15. In the third sentence replace "Appendix XS of this permit" with "40 CFR 60.7 and Figure 1 attached to this permit".

Subsection B. NSPS Storage Tanks

Pages 19-20. Okeelanta requests that these emissions units be deleted and the storage tanks listed as unregulated emissions units. The tanks are between 75 and 151 m³ in size and store volatile organic liquids with a vapor pressure less than 15.0 kPa, which makes them exempt from Subpart Kb recently revised on October 15, 2003. The previous comments, submitted prior to this subsection becoming obsolete, are listed below.

Emissions Unit Details

Page 19. Condition B.2. Change two references to EU ID No. 033 to 005.

Compliance Demonstrations and Periodic Monitoring

Page 20. Condition B.5. Change reference to Condition E.4. to Condition B.4.

Page 20. Condition B.6.b. Change paragraph (b) to delete reference to monitoring and recording of true vapor pressure. This is consistent with Section 2 of the Compliance Plan (Appendix CP-1) made part of this permit by Condition II.12.

Subsection C. Trans-shipment Facility

Page 21. <u>Brief Description.</u> Okeelanta requests that EU 026 be described as "Sugar Silos (S1101, S1102, and S1103)", and that references to EUs 027 and 028 be deleted. Since the sugar-receiving silos were designed and operate as a single system, revising the permit to one emissions unit including the silos and their three emission points is a more accurate description of the source. EUs 045, 046, and 047 should be added to this subsection.

Emissions Unit Details

Page 21. For clarification, it is suggested that the last sentence of the first paragraph be separated from the paragraph and re-worded as follows:

"The facility also includes original packaging lines and sugar grinder baghouses, refined sugar-receiving silos, a new powdered sugar dryer/cooler with baghouse, a new sugar grinder with baghouse, and new packaging lines with baghouse."

- Page 21. The last sentence of the second paragraph should be deleted since the new packaging lines (EU 047) have no connection to the existing packaging lines (EU 019).
- Page 21. The last sentence of the third paragraph should be deleted since the new powdered sugar dryer/cooler with baghouse (EU 045) has no connection to the existing sugar grinder and hopper (EU 020).
- Page 21. Designate silos S1101, S1102, and S1103 as EU 026, and delete reference to EUs 027 and 028. Add descriptions for EUs 045, 046, and 047.

Construction Restrictions

Page 22. Condition C.1. Please delete this condition since this is referring to control equipment specifications which are detailed in the construction application, but have no basis for being permit conditions. If this condition is retained, change both EUs 027 and 028 to 026 in the table. Add descriptions and information for EUs 045, 046, and 047.

Essential Potential to Emit (PTE) Parameters

Page 23. Condition C.2. Change EUs 027 and 028 to 026. Add EU 047 with process capacity of 865 tons/day. Add note at the bottom of the table to indicate that the daily process capacity of 865 tons/day for EUs 019 and 047 is the combined capacity for all packaging lines. Change note (1) for EU 019 to "Maximum Loading to packaging lines 1 through 9."

Page 23. Condition C.3(b). Change to authorize 9 original packaging lines (EU 019) and in addition four new packaging lines (EU047) to operate simultaneously up to the maximum process rate (865 tons/day) specified in Condition C.2.

Page 23. Condition C.3(c). Change to authorize operation of new sugar grinder and hopper (EU 046) in addition to original grinder and hopper (EU 020).

Page 23. Condition C.3(e). Add to authorize operation of new powdered sugar dryer/cooler (EU 045).

Page 23. Condition C.4. Add references to EUs 045, 046, and 047 in authorization to operate continuously.

Emission Limitations and Standards

Page 24. Condition C.5. Delete reference to EUs 027 and 028, and add EUs 045, 046, and 047.

Page 24. Condition C.6. Change EU 019 limit to 3.754 TPY. Change EU 020 limit to 0.060 TPY. Add EU 045 (3.379 TPY), EU 046 (0.676 TPY), and EU 047 (2.253 TPY). (See Attachment OC-EU2-F1.8 submitted with Okeelanta's renewal application to revise the permit for calculations of potential annual emissions from each unit.)

Compliance Demonstration and Periodic Monitoring

Page 25. Condition C.11. Okeelanta requests that the words "silo loaded" be deleted from paragraph (d). Okeelanta requests that the Title V permit be revised to allow recording of the total amount of sugar transferred to the three silos on a 24-hour basis. There is no corresponding condition in the underlying construction permit (Permit No. 0990005-008-AC) that would require recording sugar transferred to each individual silo. This is consistent with the Compliance Plan (Appendix CP-1) made part of this permit by Condition II.12.

Subsection D. Sugar Refinery

Brief Decription

Page 26. Change Wet Cyclone No. 1 and No. 2 to Wet Rotoclone No. 3 and No. 4, respectively, to reflect the recent changes to the facility.

Emissions Unit Details

Page 26. Replace 'wet cyclones" with "wet rotoclones" and number appropriately. Update stack heights.

Page 26. Comment III.D. The last paragraph describing EU 035 states incorrectly that the transfer bulk load-out operation is fed from the other bulk load-out operation (EU 034). The description should state that the four enclosed conveyors in series feed sugar from the refinery (curing bins or refined sugar storage silo).

Construction Restrictions

Page 27. Condition D.1. Please delete this condition since this is referring to control equipment specifications which are detailed in the construction application, but have no basis for being permit conditions.

Page 27. Condition D.1(b). If this condition is retained, the cyclonic control devices include specifications for water injection rate and pressure drop. The specifications should be identical to those identified in the permit application dated October, 2004, to replace the refinery wet cyclones. However, the cyclonic control device values were either based on stack tests of manufacturer's design data. Furthermore, measuring the pressure drop continually in these control devices has proven to be impractical due to fouling in the instrument sample lines. Okeelanta has requested that the pressure drop column be deleted and that only the water injection rate be included in the construction restrictions conditions. The minimum water injection rates should be changed to 2 gpm for EUs 021, 022, 023 and 024. This request is consistent with Section 6 of the Compliance Plan (Appendix CP-1) in the Title V permit and the January 2003 conference call with FDEP and Okeelanta.

Essential Potential to Emit (PTE) Parameters

Page 28. Condition D.2. The process rate capacity table is incorrect. There is no basis in the underlying construction permits to impose an hourly process rate restriction to the refinery sources. Therefore, the table should be modified as shown in the markup.

Page 29. Condition D.6(d). The maximum feed rate authorized for the fluidized bed dryer/cooler should be changed to 1,200 TPD as specified in the permit application. Construction Permit No. 0990005-005-AC, dated January 19, 2001, should be referenced.

Page 29. Condition D.7. The previous limitation on hours of operation is obsolete since Permit No. 0990005-005-AC became effective. The operation is limited instead by the new maximum process rates. All refinery equipment should be authorized to operate continuously within the established production limitations.

Emission Limitations and Standards

Page 30. Condition D.9. Particulate matter emission limitation should be changed to reflect permit No. 0990005-005-AC and the corresponding permit application. The allowable emission table should be changed as shown in the markup.

Subsection E. Material Handling (Cogeneration Facility)

Pages 32-36. Comment E. Various references to coal storage and handling should be deleted.

Subsection F. Cogeneration Boilers

Update this entire section to reflect permit no. PSD-FL-196(O).

Compliance Methods and Reporting

Page 48. Comment F.20.b. Mercury emissions are tested annually based on specific condition III.19.b. of permit no. PSD-FL-196(O). Based on the actual test data presented in the following table, the mercury emissions from the cogeneration boiler range between 2.66E-07 to 3.68E-06 lb/MMBtu, well below the mercury emission limit of 5.4x10⁻⁶ lb/MMBtu. Based on the consistency of actual emissions, which are well below the allowable emissions, it is requested that mercury be removed from the annual testing requirement. Based on Condition F.20, mercury emissions will be tested every 5 years upon permit renewal. In addition, it should only be required to test one of the three boilers, since all boilers are identical and are burning the same fuel from a common fuel supply.

		sting: 02/12/02 chanical Dust			Stack Testing: 01/21/03 - 01/23/03 Post-Mechanical Dust Collectors			sting: 02/11/04 chanical Dust		Stack Testing: 02/22/05 - 02/24/05 Post-Mechanical Dust Collectors			
	Unit A	Unit B	Unit C	Unit A	Unit B	Unit C	Unit A	Unit B	Unit C	Unit A	Unit B	Unit C	
Pollutant	Biomass	Biomass	Biomass	Biomass	Biomass	Biomass .	Biomass	Biomass	Biomass	Biomass	Biomass	Biomass	
	(lb/MMBtu)	(lb/MMBtu)	(lb/MMBtu)	(lb/MMBtu)	(lb/MMBtu)	(lb/MMBtu)	(lb/MMBtu)	(lb/MMBtu)	(lb/MMBtu)	(lb/MMBtu)	(lb/MMBtu)	(lb/MMBtu)	
Particulate (TSP)	0.008	0.010	0.011	0.0089	0.0079	0.0081	0.0068	0.0098	0.0123	0.0162	0.0145	0.0123	
Particulate (PM ₁₀)	0.008	0.010	0.011					, ~~	74				
VOCs	0.007	0.036	0.020	0.0027	0.0057	0.058	0.0057	0.0067	0.0063	0.0013	0.0190	0.0063	
Lead	2.08E-05	1.41E-05	2.09E-05						- ₩				
Mercury	1.65E-06	9.70E-07	3.68E-06	7.55E-07	8.51E-07	1.10E-06	6.24E-07	3.51E-07	6.14E-07	2.66E-07	1.32E-06	6.14E-07	

Sources: Air Consulting Engineering, Inc., 2005; Golder, 2005 Note: Biomass firing consisted of approximately 50% wood and 50% bagasse.

Subsection G. Paint Booth

Update this entire section to reflect permit no. 0990005-015-AC.

Page 52. Comment G.2. Delete third and fourth sentences of "Methods of Operation" paragraph to allow different manufacturers and models of the airless paint spray system as long as the airless application system is of equivalent or better efficiency.

Subsection H. Common Conditions

EU ID No., Status and Brief Description

Page 56. Comment H(1). The status and description of the retired mill boilers (EUs 003 through 013) should indicate "N/A" and "Shutdown", consistent with Section I.B. (Pages 4 and 5).

Page 56. Comment H(2). Okeelanta has requested that EUs 027 and 028 be re-designated as part of EU 026. Please refer to Comment I.B(1) above.

Page 56. Comment H(3). The Transfer Bulk load-out Operation EU ID No. should be corrected to 035. EUs 045, 046, 047, and 048 should be added to the list.

SECTION IV. ATTACHMENTS

Please include Appendix CP-1, Compliance Plan made part of the permit by Facility-wide Condition II.12.

Appendix RBL-001 Comment. This appendix should be updated to include the most recent BACT determinations for EU 014 on October 29, 2001.

Appendix U-1 Comment. The last two sections of unregulated emissions units and/or activities in this appendix (Cogeneration Facility and Trans-shipment Facility) should be assigned new ID numbers that are not assigned to other emissions units listed on Page 4 of the permit.

TABLE OF CONTENTS

Table of Contents Comment. Suggest referencing Section III.C. as "Trans-shipment facility" and Section III.D. as "Sugar Refinery". The page number column information needs to be updated. Please list Appendix CP-1, Compliance Plan.

ATTACHMENT OC-EU3-C15

EMISSION POINT INFORMATION

ATTACHMENT OC-EU1-C15

EMISSION POINT INFORMATION

Descriptions of Emissions Points Comprising this Emissions Unit:

- ID 021 Rotary Dryer/Wet Rotoclone No. 1
 - 022 Conveying/Wet Rotoclone No. 2
 - 023 Cooler No. 1/Wet Rotoclone No. 3
 - 024 Cooler No. 2/Wet Rotoclone No. 4
 - 025 Fluidized Bed Dryer/Cooler
 - 034 Bulk Load-out Operation
 - 035 Transfer Bulk Load-out Operation

Emission Point Comment:

- 1. Identification of Point on Plot Plan or Flow Diagram:
 - Bulk Load-Out Area
 - Transfer Bulk Load-Out Area
 - R3 Cooler No. 1/Wet Rotoclone No. 3
 - R4 Cooler No. 2/Wet Rotoclone No. 4
 - Fluidized Bed Dryer/Cooler Baghouse
 - R1 Rotary Dryer/Wet Rotoclone No. 1
 - R2 Conveying/Wet Rotoclone No. 2
- 14. Emission Point Comment: Stack parameters above represent average for Cooler No. 1 and No. 2 Wet Rotoclones. This emission unit has five vertical stacks serving individual control equipment and two fugitive emissions sources.

See the following table for stack/vent information for each emission point.

Stack Parameters for the Okeelanta Sugar Refinery

		Stack Height	Exit Diameter	Stack Temp	Actual Volumetric Flow Rate	Percent Water Vapor	Maximum Dry Standard Flow Rate
EU ID	Stack Description	(ft)	(ft)	(°F)	(acfm)	(%)	(dscfm)
021	Wet Rotoclone No. 1	93 (a)	2.5	100	15,000	NA	NA
022	Wet Rotoclone No. 2	93 (a)	2.5	90	15,000	NA	NA
023	Wet Rotoclone No. 3	93 (a)	2.5	100	15,000	NA	NA
024	Wet Rotoclone No. 4	93 (a)	2.5	100	15,000	NA ·	NA
025	Fluidized Bed Baghouse	80	7	115	70,620	0.7	64,390

Footnote:

(a) Estimated height based on best available information.

ATTACHMENT OC-EU2-F1.8

CALCULATION OF EMISSIONS

Attachment OC-EU3-F1.8a. Annual and Short Term Particulate Matter Emissions from Okeelanta Sugar Refinery Using the Fluidized Bed Drying System (Revised 10/14/2004)

Source Emission Point Description	Emission Unit ID		ximum Refin gar Throughp (lb/hr)	•	PM Uncontrolled Emission Factor	Loading to Control Equipment (lb/hr)	Control Efficiency (%)	Maximum Emission Rate (lb/hr)	Maximum Annual Emissions (TPY)
· · · · · · · · · · · · · · · · · · ·							Particulate M	fatter (PM)	
Fluidized Bed Baghouse	025	1,200	100,000	390,000	1.5 % ª	1,500.0	99.80 ^b	3.00	11.70
AAF Skimmer/Wet Rotoclone No.1	021	1,200	100,000	390,000	0.2090 lb/ton ^c	10.45	99.90 ^d	0.0105	0.041
AAF/ Wet Rotoclone No.2	022	1,200	100,000	390,000	0.9407 lb/ton ^c	47.03	99.90 ^d	0.0470	0.183
							Total	3.01	11.74
							Particulate M	atter (PM ₁₀)	
Fluidized Bed Baghouse	025	1,200	100,000	390,000	0.060 % ^e	60.0	99.80 ^b	0.120	0.4680
AAF Skimmer/Wet Rotoclone No.1	021	1,200	100,000	390,000	0.00836 lb/tone	0.418	99.00 ^d	0.00418	0.0163
AAF/ Wet Rotoclone No.2	022	1,200	100,000	390,000	0.03763 lb/ton ^e	1.881	99.00 ^d	0.01881	0.0734
						_	Total	0.124	0.48

Footnotes:

Formula used with multiple for drop points, Rotoclone No. 1 having 2 drop points and Rotoclone No. 2 with 9 drop points.

E (lb/ton) = $k \times 0.0032 \times (U/5)^1.3 / (M/2)^1.4$; where U is assumed to be a max of 1 mph due to the building enclosure.

M = Moisture Content = 0.03% for refined sugar.

k = 0.74 for PM

E = 0.104 lb/ton per transfer point/operation, or 0.941 lb/ton for 9 points.

^a Based on manufacturers maximum estimated PM inlet loading rate of 1.5 % of throughput rate for fluidized bed dryer/cooler. Factor assumes that all of the fluidized bed dryer/cooler sugar dust is vented to this control device.

^b Baghouse manufacturers efficiency.

^c Based on continuous drop emission factors computed from AP-42 (USEPA, 1995) Section 13.2.4.

^d Manufacturers control equipment efficiency rating for total PM = 99.9% and PM₁₀ = 99.0%.

^e Based on sugar dust analysis, uncontrolled PM₁₀ is less than 4% of total sugar dust loading to the control equipment.

Attachment OC-EU3-F1.8b. Annual and Short Term Particulate Matter Emissions from Okeelanta Sugar Refinery Using the Rotary Drying System (Revised 10/14/2004)

(Note: This operating scenario represents the worst-case short-term particulate emissions.)

Source Emission Point Description	Emission Unit ID	ID Sugar Throughput			PM Uncontrolled Emission	Loading to Control Equipment	Control Efficiency ^c	Maximum Emission Rate	Maximum Annual Emissions
· · · · · · · · · · · · · · · · · · ·		(TPD)	(lb/hr)	(TPY)	Factor	(lb/hr)	(%)	(lb/hr)	(TPY)
							Particulate Ma	tter (PM)	
Cooler No. 1 /Rotoclone No. 3	023	1,200	100,000	130,000	0.175 % a	175	99.9	0.17	0.23
Cooler No. 2 /Rotoclone No. 4	024	1,200	100,000	130,000	0.175 % a	175	99.9	0.17	0.23
AAF Skimmer/Wet Rotoclone No.1 (from dryer)	021	1,200	100,000	130,000	3.150 % a	3,150	99.9	3.15	4.09
AAF Skimmer/Wet Rotoclone No.1 (from transfer points)	021	1,200	100,000	130,000	0.2090 lb/ton ^b	10.45	. 99.9	0.0105	0.014
AAF/Wet Rotoclone No.2	022	1,200	100,000	130,000	0.9407 lb/ton ^b	47.03	99.9	0.0470	0.061
							Total	3.56	4.62
							Particulate Mat	ter (PM ₁₀)	
Cooler No. 1 /Rotoclone No. 3	023	1,200	100,000	130,000	0.007 % ^d	7.0	99.0	0.07	0.09
Cooler No. 2 /Rotoclone No. 4	024	1,200	100,000	130,000	0.007 % d	7.0	99.0	0.07	0.09
AAF Skimmer/Wet Rotoclone No.1 (from dryer)	021	1,200	100,000	130,000	0.126 % ^d	126.0	99.0	1.26	1.64
AAF Skimmer/Wet Rotoclone No.1 (from transfer points)	021	1,200	100,000	130,000	0.00836 lb/tond	0.418	99.0	0.0042	0.005
AAF/Wet Rotoclone No.2	022	1,200	100,000	130,000	0.03763 lb/ton ^d	1.881	99.0	0.0188	0.024
· · ·							Total	1.42	1.85

Footnotes:

 $k \approx 0.74$ for PM

E = 0.104 lb/ton per transfer point/operation, or 0.941 lb/ton for 9 points.

^a Based on sugar industry data, uncontrolled sugar dust loading (PM and PM₁₀) is a max of 3.5% of the total refined sugar throughput when rotary dryers/coolers are used. Factor assumes that 5% of the uncontrolled sugar dust is vented to each Cooler No. 1 and No. 2 Wet Cyclone and 90% is vented to Wet Rotoclone No. 1.

b Wet Rotoclone No. 1 controls 2 transfer points/operations; wet Rotoclone No. 2 controls 9 transfer points/operations. Continuous/batch drop equation from AP-42 (USEPA, 1995) Section 13.2.4. Formula used with multiple for drop points, Rotoclone No. 1 having 2 drop points and Rotoclone No. 2 with 9 drop points. E (lb/ton) = k x 0.0032 x (U/5)^1.3 / (M/2)^1.4; where U is assumed to be a max of 1 mph due to the building enclosure.

M = Moisture Content = 0.03% for refined sugar.

^c Manufacturers control equipment efficiency rating for total PM = 99.9% and PM₁₀ = 99.0%.

^d Based on sugar dust analysis, uncontrolled PM₁₀ is less than 4% of total sugar dust loading to the control equipment.

Attachment OC-EU3-F1.8c. Annual and Short Term Particulate Matter Emissions from Okeelanta Sugar Refinery

Using the Combination of the Fluidized Bed Drying System and the Rotary Drying System (revised 10/14/2004)

Source Emission	Emission	Refined Sugar			PM Uncontrolled	Loading to Control	Control	Maxi Emis	
Point Description	Unit ID		Throughput '	a	Emission	Equipment	Efficiency	Ra	ite
· · · · · · · · · · · · · · · · · · ·		(TPD)	(lb/hr)	(TPY)) Factor	(lb/hr)	(%)	(lb/hr)	(TPY)
							Particulate Ma	atter (PM)	
Fluidized Bed Drying System									
Fluidized Bed Baghouse	025	1,050	87,500	260,000	1.5 %	1312.5	99.8	2.63	7.80
Rotary Drying System									
Cooler No. 1 / Rotoclone No. 3	023	450	37,500	130,000	0.175 %	65.63	99.9	0.07	0.23
Cooler No. 2 / Rotoclone No. 4	024	450	37,500	130,000	0.175 %	65.63	99.9	0.07	0.23
AAF Skimmer/Wet Rotoclone No.1 (from dryer)	021	450	37,500	130,000	3.150 %	1,181.3	99.9	1.18	4.09
Material Handling									
AAF Skimmer/Wet Rotoclone No.1 (from transfer points)	021	1,500	125,000	390,000	0.2090 lb/ton	13.06	99.9	0.0131	0.0408
AAF/Wet Rotoclone No.2	022	1,500	125,000	390,000	0.9407 lb/ton	58.79	99.9	0.0588	0.1834
		-,	,						
							Total	4.01	12.57
							Particulate Ma	tter (PM ₁₀)	
Fluidized Bed Drying System								. 107	•
Fluidized Bed Baghouse	025	1,050	87,500	260,000	0.060 %	52.50	99.8	0.105	0.31
1									
Rotary Drying System									
Cooler No. 1 / Rotoclone No. 3	023	450	37,500	130,000	0.007 %	2.63	99.0	0.03	0.09
Cooler No. 2 / Rotoclone No. 4	024	450	37,500	130,000	0.007 %	2.63	99.0	0.03	0.09
AAF Skimmer/Wet Rotoclone No.1 (from dryer)	021	450	37,500	130,000	0.126 %	47.25	99.0	0.47	1.64
Material Handling									
AAF Skimmer/Wet Rotoclone No.1 (from transfer points)	021	1,500	125,000	390,000	0.00836 lb/ton	0.523	99.0	0.0052	0.0163
AAF/Wet Rotoclone No.2	022	1,500	125,000	390,000	0.03763 lb/ton	2.352	99.0	0.0235	0.0734
							Total	0.63	2.22

Note: See Attachments OC-EU3-G8a and OC-EU3-G8b for footnotes concerning emission factors and control efficiencies.

^a Based on 1,500 tons/day (TPD) throughput as a combined operation potential maximum for the refinery.

Attachment OC-EU3-F1.8d. Annual and Short Term Particulate Matter Emissions from Okeelanta Sugar Refinery Bulk and Transfer Load-out Operations (Revised 10/14/04)

Source Emission Point Description	Emission Unit ID	R	Maximum tefined Suga Throughput ^a		PM Uncontrolled Emission	Uncontrolled PM Emissions	Control Efficiency	Maximum Emission Rate	Annual Emissions
rome Description	- Cill ID	(TPD)	(lb/hr)	(TPY)	Factor	(lb/hr)	(%)	(lb/hr)	(TPY)
							Particulate M	atter (PM)	
Bulk load-out Operations	034	600	88,000	117,000	0.105 lb/ton ^b	4.60	50 ^d	2.30	3.06
Transfer Bulk Load-out Operations	035	1,200	144,000	273,000	0.105 lb/ton ^b	7.53	90 ^d	0.75	1.43
						_	Total	3.05	4.48
					,		Particulate Ma	atter (PM ₁₀)	
Bulk load-out Operations	034	600	88,000	117,000	0.00418 lb/ton ^c	0.184	50 ^d	0.092	0.12
Transfer Bulk Load-out Operations	035	1,200	144,000	273,000	0.00418 lb/ton ^c	0.301	90 ^d	0.030	0.06
						. –	Total	0.122	0.18

Throughput based on 1,800 tons/day (TPD) and 390,000 tons/yr (TPY), with 30/70% split between the Bulk and Transfer Bulk load-out operations.

^b Bulk load-out operations continuous drop emission factors are computed from AP-42 (USEPA, 1995) Section 13.2.4.

E (lb/ton) = $k \times 0.0032 \times (U/5)^{1.3} / (M/2)^{1.4}$; where U is assumed to be a max of 1 mph due to the building enclosure.

M = Moisture Content = 0.03% for refined sugar.

k = 0.74 for PM

^c PM₁₀, based on sugar dust analysis, is less than 4% of total sugar dust loading.

^d Represents assumed control efficiency achieved from the building load-out enclosure. Transfer bulk load-out control efficiency is higher than bulk load-out building due to improved design and operating procedures.

Attachment OC-EU3-F1.8e. Summary of Maximum Annual and Short Term Particulate Matter Emissions from Okeelanta Sugar Refinery

Source Emission	Emission	Individua Maximum E		Overall M	
Point Description	Unit ID	lb/hr	TPY	lb/hr	TPY
7					
Particulate Mat	ter (PM)				
Fluidized Bed Drying System Fluidized Bed Baghouse	025	3.00	11.70	2.63	7.80
Tuddized Bed Bagnouse	023	3.00	11.70	2.03	7.60
Rotary Drying System					
Cooler No. 1 / Wet Rotoclone No. 3	023	0.17	0.23	0.07	0.23
Cooler No. 2 / Wet Rotoclone No. 4	024	0.17	0.23	0.07	0.23
AAF Skimmer/Wet Rotoclone No.1 (from dryer)	021	3.15	4.09	3.15	4.09
Material Handling					
AAF Skimmer/Wet Rotoclone No.1 (from transfer points)	021	0.01	0.04	0.01	0.04
AAF/Wet Rotoclone No.2	022	0.06	0.18	0.05	0.18
	022	0.00		0.00	0110
Bulk and Transfer Load-Out Operations					
Bulk load-out Operations	034	2.30	3.06	2.30	3.06
Transfer Bulk Load-out Operations	035	0.75	1.43	0.75	1.43
·	Total			7.06	17.06
	_ h				
Particulate Matt	er (PM ₁₀) ^b				
Fluidized Bed Drying System					
Fluidized Bed Baghouse	025	0.12	0.47		0.31
Rotary Drying System					
Cooler No. 1 / Wet Rotoclone No. 3	023	0.07	0.09	0.07	0.09
Cooler No. 2 / Wet Rotoclone No. 4	024	0.07	0.09	0.07	0.09
AAF Skimmer/Wet Rotoclone No.1 (from dryer)	021	1.26	1.64	1.26	1.64
(_			
Material Handling					
AAF Skimmer/Wet Rotoclone No.1 (from transfer points)	021	0.005	0.016	0.004	0.016
AAF/Wet Rotoclone No.2	022	0.024	0.073	0.019	0.073
Bulk and Transfer Load-Out Operations					
Bulk load-out Operations	034	0.09	0.12	0.09	0.12
Transfer Bulk Load-out Operations	035	0.03	0.06	0.03	0.06
	Total			1.54	2.40
		,			

^a Maximum emissions occur when using the combination of the Fluidized Bed and Rotary drying systems.

Maximum hourly emissions occur when using the Rotary drying system
 Maximum overall annual emissions occur when using the combination of the Fluidized Bed and Rotary drying systems.

Attachment OC-EU3-F1.8f. Annual and Short Term Emissions of VOCs from Sugar Refinery Chemical Usage

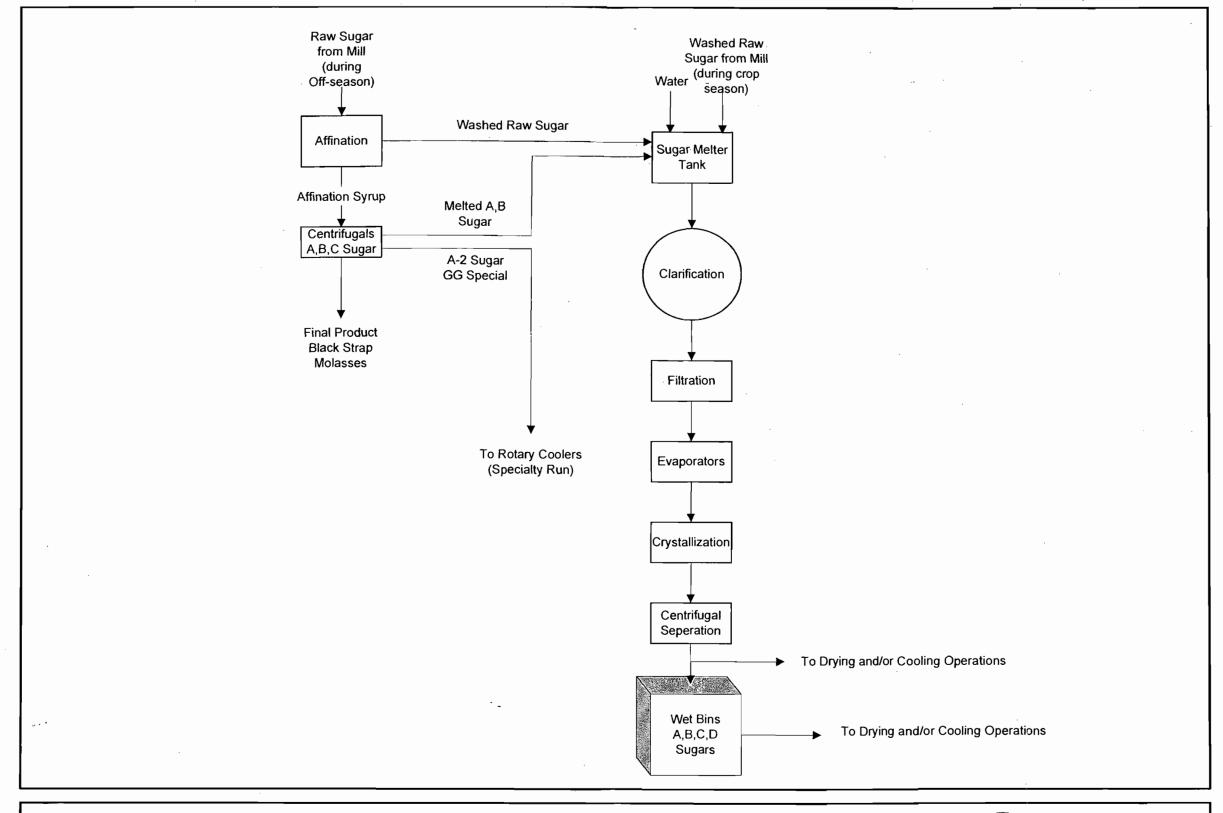
	• .		Pote	ntial
Material	Chemical	VOC Content	Chemical Usage ^a (lb/yr)	VOC Emissions (TPY)
		· .	,	
Pure Isopropyl Alcohol	Isopropyl Alcohol	100%	77,500	38.75
Rodine 213	Isopropyl Alcohol	15%	3,000	0.225
	Propargyl Alcohol	3%	3,000	0.045
		Total VOCs =	11.54 lb/hr ^b	39.02 TP

^a Based on mill estimates for maximum usage rates.

^b Based on an average 6762 hours per year for the dryers during 1998 and 1999 operation, assuming that 100% of compound is emitted to the atmosphere.

ATTACHMENT OC-EU3-I1

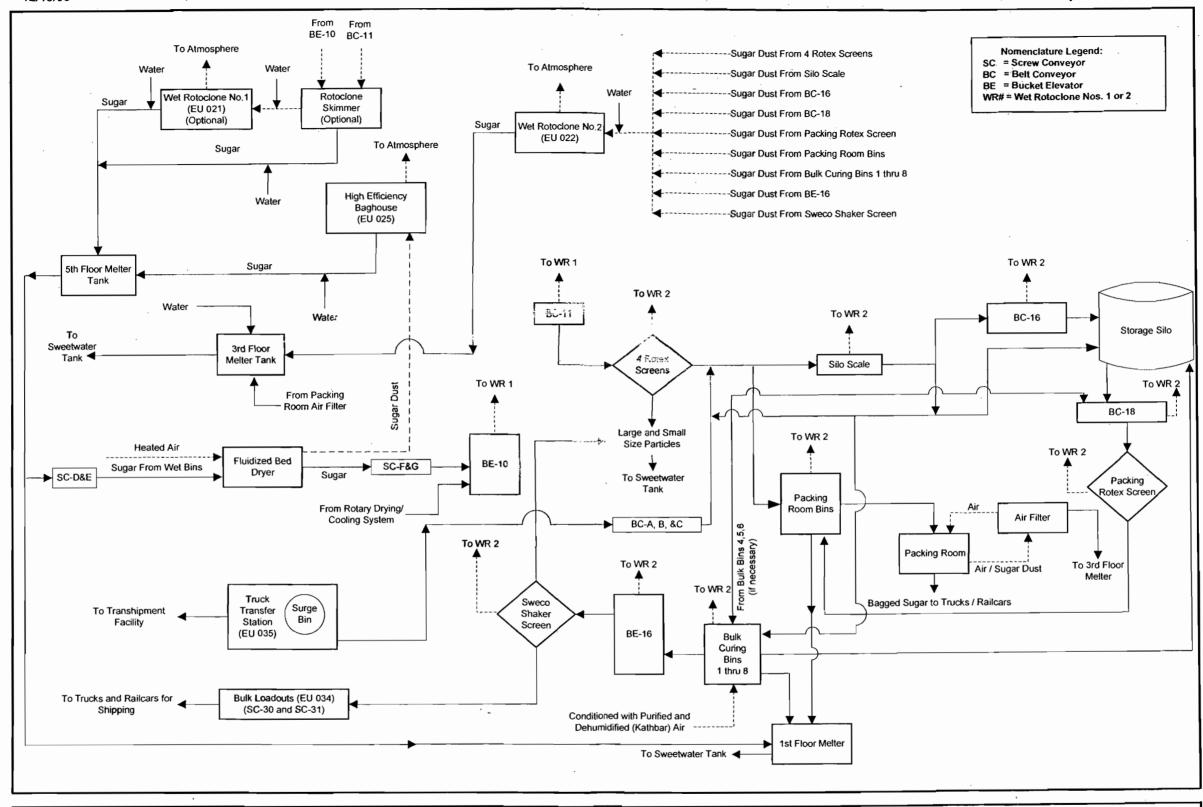
PROCESS FLOW DIAGRAM



Attachment OC-EU1-I1a. Process Flow Diagram Sugar Mill Refinery Expansion Florida Crystals Refinery South Bay, Florida

Process Flow Legend
Solid/Liquid →
Gas

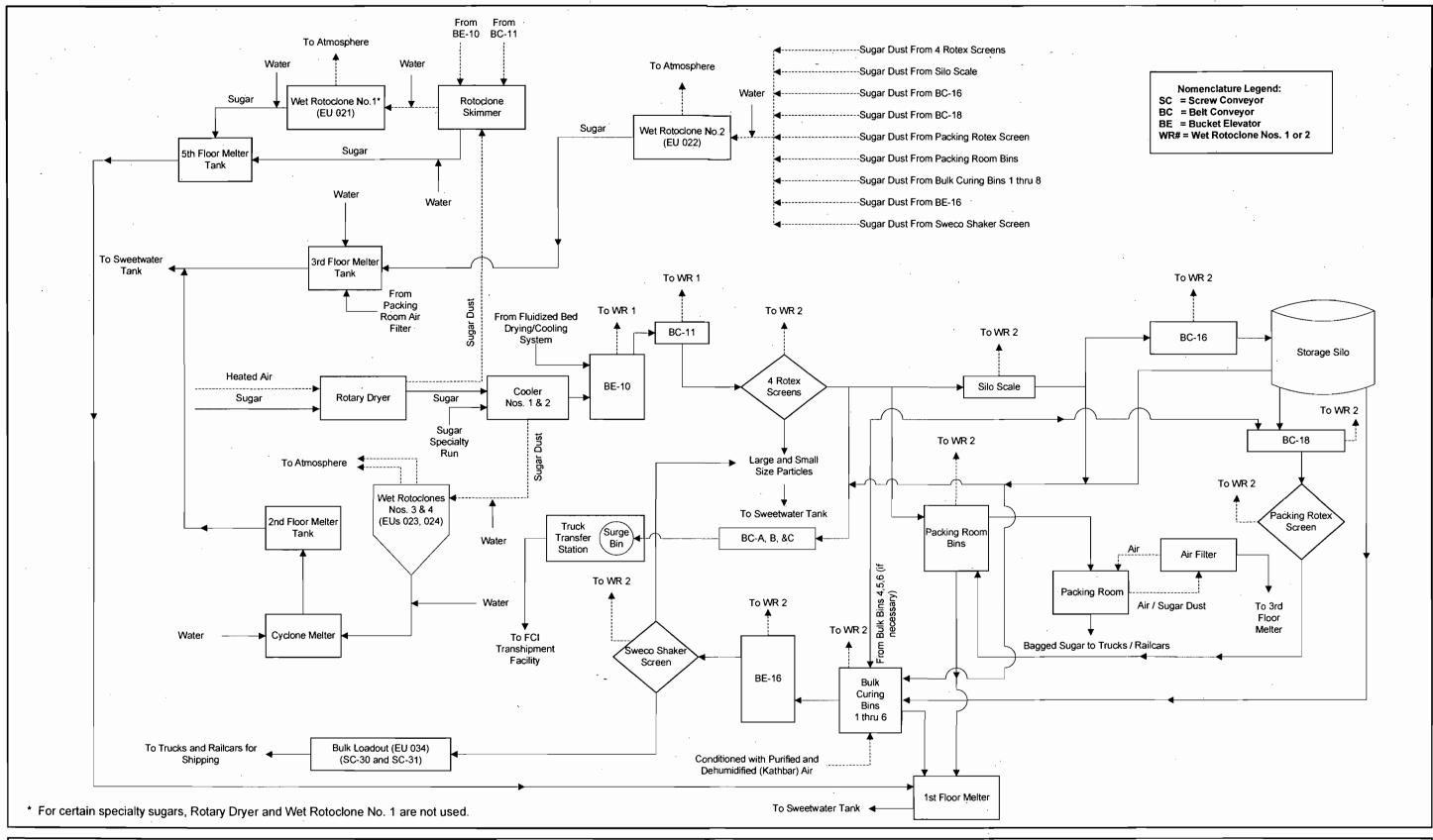




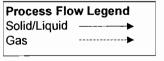
Attachment OC-EU1-I1b. Process Flow Diagram Refinery Operations with Fluidized Bed Dryer/Cooler Okeelanta Refinery South Bay, Florida

Process Flow Legend
Solid/Liquid ----Gas

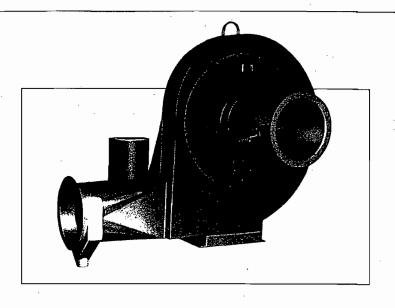




Attachment OC-EU1-I1c. Process Flow Diagram Refinery Operations with Rotary Dryer/Coolers Okeelanta Refinery South Bay, Florida







Type W RotoClone

WET CENTRIFUGAL COLLECTOR

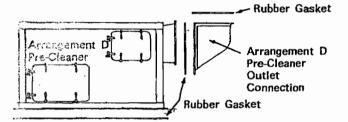
American Air Filter

		Capacity	injet	L								SYSTEM-	-INCHE	w. G.				_	
		in C.F.M.	Velocity F.P.M.	R.P.M.	B.H.P.	R.P.M.	3" B.H.P.	R.P.M.	B.H.P.		5" B.H.P.		6"	R.P.M.	P# 11 D		8"	_	9"
• • •		9000	2860	570	8.5	655	12.0	743	14.0	R.P.M. 815	18.0	R.P.M.	B.H.P. 22.0	955	B.H.P. 25.0	R.P.M.	B.H.P. 28.0	R.P.M. 1075	B.H.P. 32.0
		9500	3020	575	9.0	665	13.0	750	16.0	825	19.0	895	23.0	960	26.0	1025	29.0	1080	33.0
		10000	3180	585	11.0	675	14.0	755	17.0	830	20.0	900	24.0	965	27.0	1030	31.0	1085	35.0
		11000 12000	3500 3820	605 630	13.0	695 710	16.0	770 785	18.0	840 855	23.0	910	27.0 30.0	970	31.0	1035	35.0	1090	38.0
200		13000	4140	650	17.0	737	21.0	800	25.0	870	28.0	935	34.0	995	38.0	1055	38.0 43.0	1110	42.0 47.0
×		14000	4460	675	19.0	755	23.0	820	28.0	887	32.0	950	38.0	1010	42.0	1065	47.0	1120	51.0
اندۇر ئىزى		15000 15500	4780 4940	710	23.0 25.0	780 795	27.0	840 850	32.0 34.0	905	36.0	965	42.0	1025	46.0 49.0	1080	51.0	1130	56.0
46		13300	4940	/35	25.0	/95	29.0	830	34.0	713	39.0	9/5	44.0	1030	49.0	1085	54.0	1135	59.0
		Capacity	Infet			·						SYSTEM-							
32		C.F.M.	F.P.M.	R.P.M.	# B.i\.P.	R.P.M.	B.H.P.	R.P.M.	4" B.H.P.	R.P.M.	5" B.H.P.	R.P.M.	6" B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.
		9000	2860	655	12.0	743	14.0	815	18.0	890	22.0	955	25.0	1020	28.0	1075	32.0	1125	36.0
		9500	3020	675	13.0	760	16.0	835	19.0	900	23.0	960	26.0	1030	29.0	1090	33.0	1135	37.0
9	ROTO CLONE	10000	3180 3500	695 732	17.0	775 805	18.0	850 875	22.0 25.0	915	24.0	980	28.0 33.0	1040	33.0 37.0	1100	36.0 41.0	1145	40.0
		12000	3820	768	22.0	835	25.0	905	28.0	970	34.0	1030	38.0	1090	42.0	1140	46.0	1160	45.0 51.0
	e Historiculus	13000	4140	815	26.0	088	30.0	940	35.0	1008	39.0	1060	43.0	1115	47.0	1165	51.0	1215	55.0
	Ū.	14000	4460	853	30.0	920	35.0	980	40.0	1037	45.0	1092	49.0	1143	53.0	1198	59.0	1238	. 62.0
5		15000 15500	4780 4940	895 915	36.0 39.0	957 975	41.0	1015	46.0	1070 1185	51.0 54.0	1125	56.0	1175	61.0	1230	69.0 71.0	1273 1285	71.0 76.0
183				110			- 111	, , ,										7105	70.0
		Capacity	Inlet Velocity	2	*		·		TOTAL		RE OF	SYSTEM	-INCHES	W. G.	7	-	·	•	
		C.F.M.	F.P.M.	R.P.M.	B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.
/警	SEVERY A	12000	3020	507	12.0	587	16.0	662	19.0	727	23.0	790	28.0	850	32.0	906	38.0	958	42.0
		13000	3270 3520	523 540	13.0 16.0	600	18.0	670 680	22.0 24.0	735 745	26.0 28.0	800 805	31.0 35.0	856 860	35.0 38.0	908 915	40.0 44.0	960	46.0
	=(0)(08 HaD)(15 H	5000	3770	555	18.0	612	22.0	692	27.0	755	32.0	815	37.0	870	42.0	925	47.0	965	49.0 53.0
. 鑾	elitanigement	6000	4020	575	20.0	640	24.0	705	29.0	765	35.0	825	40.0	879	46.0	932	51.Q	978	57.0
(選/		17000	4270	590	23.0	655	27.0	716	32.0	775	38.0	832	44.0	890	50.0	940	55.0	987	62.0
8		18000 19000	4530 4780	610	26.0 29.0	675 690	31.0	730 750	36.0 40.0	790 805	42.0 46.0	843 855	48.0 52.0	900 910	54.0 58.0	950 956	59.0 64.0	992 1003	66.0
		20000	5030	650	33.0	710	35.0	762	44.0	815	50.0	870	56.0	920	63.0	968	70.0	1003	70.0 76.0
33										Daves									70.0
		Capacity :	Inlet Volocity	7	<i>"</i>	3	7		JOIAL		KE UF	SYSTEM	-INCHE		H	F	"		
1		C.F.M.	F.P.M.	R.P.M.	B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.	R.P.M.	B.H.P.
		14000 15500	2860	440	12.0	515	16.0	585	20.0	646	24.0	702	28.0	755	34.0	805	38.0	855	44.0
	THE STORY OF	17000	3160 3460	450 475	13.0 16.0	525 537	18.0 21.0	590 600	23.0 26.0	650 655	27.0 31.0	705 710	33.0 37.0	756 760	38.0 42.0	807 810	43.0 47.0	857	48.0
E.		18500	3760	490	18.0	555	24.0	615	29.0	670	35.0	718	40.0	768	46.0	813	27.0	860 863	53.0 55.0
7		20000	4070	505	22.0	568	27.0	625	33.0	680	39.0	730	45.0	775	51.0	818	27.0	865	63.0
7		21500	4380 4680	525 550	25.0 29.0	590 602	32.0 36.0	640	37.0 42.0	690	43.6	740	50.0	785	56.0	830	63.0	870	69.0
ici		24500	5000	575	34.0	620	40.0	675	47.0	705 720	48.0 54.0	750 765	55.0 62.0	795 809	62.0	840 850	69.0 75.0	881 890	76.0 83.0
200	51000000000000000000000000000000000000	25000	5090	590	36.6	630	42.0	680	49.0	725	57.0	772	64.0	815	71.0	855	78.0	895	85.0
23	EASY THE LOW	Capacity	Injet			bas.			TOTAL	PDESSII	DE DE	SYSTEM	INCHES	ws				, tr	
		in C.F.M.	Velocity F.P.M.	2	-		 		"		# OI		"	7	*				
200		Landa I								4							ا	9	-
200					B.H.P.			R.P.M.	B.H.P.	R.P.M.				R.P.M.		R.P.M.	8.H.P.	R.P.R.	S.H.P.
1		17000 18500	2860	400	15.0	470	21.0	R.P.M. 530	B.H.P. 27.0	R.P.M. 590	33.0	640	38.0	690	45.0	735	8.H.P. 51.0	R.P.R.	8.H.P. 58.0
1.		17000						R.P.M.	B.H.P.	R.P.M.						R.P.M.	8.H.P.	R.P.R.	S.H.P.
100		17000 18500 20000 21500	2860 3110 3370 3620	400 405 410 430	15.0 17.0 20.0 23.0	470 475 482 490	21.0 23.0 26.0 29.0	R.P.M. 530 535 540 550	8.H.P. 27.0 29.0 33.0 36.0	R.P.M. 590 595 600 605	33.0 36.0 39.0 43.0	640 644 648 652	38.0 42.0 46.0 50.0	690 694 697 700	45.0 49.0 53.0 58.0	R.P.M. 735 739 743 747	8.H.P. 51.0 56.0 60.0 66.0	R.P.R. 775 778 781 785	8.H.P. 58.0 65.0 68.0 74.0
N. S.		17000 18500 20000	2860 3110 3370 3620 3870	400 405 410 430 445	15.0 17.0 20.0 23.0 26.0	470 475 482 490 500	21.0 23.0 26.0 29.0 33,0	R.P.M. 530 535 540 550 558	8.H.P. 27.0 29.0 33.0 36.0 40.0	R.P.M. 590 595 600 605 610	33.0 36.0 39.0 43.0 47.0	640 644 648 652 656	38.0 42.0 46.0 50.0 55.0	690 694 697 700 705	45.0 49.0 53.0 58.0 64.0	735 739 743 747 750	8.H.P. 51.0 56.0 60.0 66.0 72.0	775 778 781 785 790	8.H.P. 58.0 65.0 68.0 74.0 79.0
化工程的工 业		17000 18500 20000 21500 23000	2860 3110 3370 3620	400 405 410 430	15.0 17.0 20.0 23.0	470 475 482 490	21.0 23.0 26.0 29.0	R.P.M. 530 535 540 550	8.H.P. 27.0 29.0 33.0 36.0	R.P.M. 590 595 600 605	33.0 36.0 39.0 43.0	640 644 648 652	38.0 42.0 46.0 50.0	690 694 697 700	45.0 49.0 53.0 58.0	R.P.M. 735 739 743 747	8.H.P. 51.0 56.0 60.0 66.0 72.0 77.0	R.P.R. 775 778 781 785	8.H.P. 58.0 65.0 68.0 74.0 79.0 85.0
机型器性间歇		17000 18500 20000 21500 23000 24500 26000 27500	2860 3110 3370 3620 3870 4125 4370 4625	400 405 410 430 445 460 475 490	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0	470 475 482 490 500 512 525 537	21.0 23.0 26.0 29.0 33,0 37.0 41.0 46.0	R.P.M. 530 535 540 550 558 568 575 587	8.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 54.0	R.P.親. 590 595 600 605 610 615 625 635	33.0 36.0 39.0 43.0 47.0 52.0 57.0 63.0	640 644 648 652 656 662 668 678	38.0 42.0 46.0 50.0 55.0 60.0 66.0 72.0	690 694 697 700 705 710 715 720	45.0 49.0 53.0 58.0 64.0 69.0 74.0 80.0	R.P.M. 735 739 743 747 750 753 756 762	8.H.P. 51.0 56.0 60.0 66.0 72.0 77.0 82.0 89.0	R.P.M. 775 778 781 785 790 795 800 805	8.H.P. 58.0 65.0 68.0 74.0 79.0 85.0 91.0 99.0
		17000 18500 20000 21500 23000 24500 26000	2860 3110 3370 3620 3870 4125 4370	400 405 410 430 445 460 475	15.0 17.0 20.0 23.0 26.0 29.0 34.0	470 475 482 490 500 512	21.0 23.0 26.0 29.0 33,0 37.0 41.0	R.P.M. 530 535 540 550 558 568 575	8.H.P. 27.0 29.0 33.0 36.0 40.0 44.0	R.P.M. 590 595 600 605 610 615	33.0 36.0 39.0 43.0 47.0 52.0	640 644 648 652 656 662	38.0 42.0 46.0 50.0 55.0 60.0	690 694 697 700 705 710	45.0 49.0 53.0 58.0 64.0 69.0 74.0	R.P.M. 735 739 743 747 750 753 756	8.H.P. 51.0 56.0 60.0 66.0 72.0 77.0 82.0	R.P.M. 775 778 781 785 790 795 800	8.H.P. 58.0 65.0 68.0 74.0 79.0 85.0 91.0
		17000 18500 20000 21500 23000 24500 26000 27500 29000	2860 3110 3370 3620 3870 4125 4370 4625 4880	400 405 410 430 445 460 475 490 510	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0	470 475 482 490 500 512 525 537 550	21.0 23.0 26.0 29.0 33,0 37.0 41.0 46.0 51.0	R.P.M. 530 535 540 550 558 568 575 587 600	8.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 54.0 59.0	R.P.R. 590 595 600 605 610 615 625 635 640 PRESSU	33.0 36.0 39.0 43.0 47.0 52.0 57.0 63.0 68.0	640 644 648 652 656 662 668 678 688	38.0 42.0 46.0 50.0 55.0 60.0 66.0 72.0 77.0	690 694 697 700 705 710 715 720 728	45.0 49.0 53.0 58.0 64.0 69.0 74.0 80.0 86.0	R.P.M. 735 739 743 747 750 753 756 762	8.H.P. 51.0 56.0 60.0 66.0 72.0 77.0 82.0 89.0	R.P.M. 775 778 781 785 790 795 800 805 810	8.H.P. 58.0 65.0 68.0 74.0 79.0 85.0 91.0 99.0
		17000 18500 20000 21500 23000 24500 26000 27500 29000	2860 3110 3370 3620 3870 4125 4370 4625 4880	400 405 410 430 445 460 475 490 510	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0	470 475 482 490 500 512 525 537 550	21.0 23.0 26.0 29.0 33,0 37.0 41.0 46.0 51.0	R.P.M. 530 535 540 550 558 568 575 587 600	8.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 54.0 59.0	R.P.R. 590 595 600 605 610 615 625 635 640 PRESSU	33.0 36.0 39.0 43.0 47.0 52.0 57.0 63.0 68.0	640 644 648 652 656 662 668 678 688	38.0 42.0 46.0 50.0 55.0 60.0 66.0 72.0 77.0	690 694 697 700 705 710 715 720 728 W. G.	45.0 49.0 53.0 58.0 64.0 69.0 74.0 80.0 86.0	R.P.M. 735 739 743 747 750 753 756 762 768	8.H.P. 51.0 56.0 60.0 66.0 72.0 77.0 82.0 89.0 96.0	R.P.E. 775 778 781 785 790 795 800 805 810	8.H.P. 58.0 65.0 68.0 74.0 79.0 85.0 91.0 99.0 106
		17000 18500 20000 21500 23000 24500 24500 27500 29000	2860 3110 3370 3620 3870 4125 4370 4625 4880 Inlet Velocity	400 405 410 430 445 460 475 490 510	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0	470 475 482 490 500 512 525 537 550	21.0 23.0 26.0 29.0 33,0 37.0 41.0 46.0 51.0	R.P.M. 530 535 540 550 558 568 575 587 600	8.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 54.0 59.0	R.P.R. 590 595 600 605 610 615 625 635 640 PRESSU	33.0 36.0 39.0 43.0 47.0 52.0 57.0 63.0 68.0	640 644 648 652 656 662 668 678 688	38.0 42.0 46.0 50.0 55.0 60.0 66.0 72.0 77.0	690 694 697 700 705 710 715 720 728	45.0 49.0 53.0 58.0 64.0 69.0 74.0 80.0 86.0	R.P.M. 735 739 743 747 750 753 756 762 768	8.H.P. 51.0 56.0 60.0 66.0 72.0 77.0 82.0 89.0 96.0	R.P.M. 775 778 781 785 790 795 800 805 810	8.H.P. 58.0 65.0 68.0 74.0 79.0 85.0 91.0 99.0
		17000 18500 20000 21500 23000 24500 24500 27500 29000 CapscRy in C.F.M.	2860 3110 3370 3620 3870 4125 4370 4625 4880 hniet Welocity F.P.M. 2830 3110	400 405 410 430 445 460 475 490 510 2 R.P.M. 362 375	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0	470 475 482 490 500 512 525 537 550 3 R.P.M. 425 435	21.0 23.0 26.0 29.0 33.0 37.0 41.0 46.0 51.0	R.P.M. 530 535 540 550 558 568 575 587 600 4 R.P.M. 485 490	B.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 54.0 59.0 TOTAL # B.H.P. 31.0 35.0	R.P.M. 590 595 600 605 610 615 625 635 640 PRESSU 5 R.P.M. 540	33.0 36.0 39.0 43.0 47.0 52.0 57.0 68.0 RE OF : " B.H.P. 38.0 43.0	640 644 648 652 656 662 668 678 688 SYSTEM- 6 R.P.M. 587	38.0 42.0 44.0 50.0 55.0 60.0 72.0 77.0 -INCHES	690 694 697 700 705 710 715 720 728 W. G.	45.0 49.0 53.0 58.0 64.0 69.0 74.0 80.0 86.0	R.P.M. 735 739 743 747 750 753 756 762 768	8.H.P. 51.0 56.0 60.0 66.0 72.0 77.0 82.0 89.0 96.0	R.P.M. 775 778 781 785 790 795 800 805 810 9 R.P.M. 710 712	8.H.P. 58.0 65.0 68.0 74.0 79.0 85.0 91.0 99.0 106
		17000 18500 20000 21500 23000 24500 24500 27500 29000 CapscRy in C.F.MI. 20000 22000 24000	2860 3110 3370 3620 3870 4125 4370 4625 4880 Inlet Velocity F.P.M. 2830 3110 3400	400 405 410 430 445 460 510 510 2 R.P.M. 362 375 388	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0	470 475 482 490 500 512 525 537 550 3 R.P.M. 425 435	21.0 23.0 26.0 29.0 33.0 37.0 41.0 46.0 51.0	R.P.M. 530 535 540 550 558 568 575 587 600 4 R.P.M. 485 490 500	B.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 54.0 59.0 TOTAL "B.H.P. 31.0 35.0 39.0	R.P.M. 590 595 600 605 610 615 625 635 640 PRESSU 540 545 550	33.0 36.0 39.0 43.0 47.0 52.0 57.0 68.0 RE OF : " B.H.P. 38.0 43.0	640 644 648 652 656 662 668 678 688 678 688 678 587 597 592 596	38.0 42.0 46.0 50.0 55.0 60.0 66.0 72.0 77.0 INCHES 77 8.H.P. 45.0 51.0 56.0	690 694 697 700 705 710 715 720 728 W. G. 7 R.P.M. 630 635 640	45.0 49.0 53.0 58.0 64.0 69.0 80.0 86.0 88.H.P. 54.0 65.0	R.P.M. 735 739 743 747 750 753 756 762 768 R.P.M. 675 675 680	8.H.P. 51.0 56.0 60.0 66.0 72.0 77.0 82.0 89.0 96.0	R.P.M. 775 778 781 785 790 795 800 805 810 9 R.P.M. 710 712 720	8.H.P. 58.0 65.0 68.0 74.0 79.0 85.0 91.0 99.0 106 8.H.P. 69.0 76.0 83.0
		17000 18500 20000 21500 23000 24500 24500 27500 29000 CapscRy in C.F.M.	2860 3110 3370 3620 3870 4125 4370 4625 4880 hniet Welocity F.P.M. 2830 3110	400 405 410 430 445 460 475 490 510 2 R.P.M. 362 375	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0	470 475 482 490 500 512 525 537 550 3 R.P.M. 425 435 440	21.0 23.0 26.0 29.0 33.0 37.0 41.0 46.0 51.0	R.P.M. 530 535 540 550 558 568 575 587 600 4 R.P.M. 485 490	B.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 54.0 59.0 TOTAL # B.H.P. 31.0 35.0	R.P.M. 590 595 600 605 610 615 625 635 640 PRESSU 5 R.P.M. 540 545 550	33.0 36.0 39.0 43.0 47.0 52.0 57.0 63.0 68.0 RE OF : "B.H.P. 38.0 48.0	640 644 648 652 656 668 678 688 SYSTEM 6 7 8.P.M. 587 592 596 600	38.0 42.0 46.0 50.0 55.0 60.0 77.0 77.0 B.H.P. 45.0 56.0 62.0	690 694 697 700 705 710 715 720 728 W. G. 728 630 635 640	45.0 49.0 53.0 58.0 64.0 69.0 80.0 86.0 88.0 54.0 55.0 72.0	R.P.M. 735 739 743 747 750 753 756 762 768 8 R.P.M. 675 675 680 685	8.H.P. 51.0 56.0 60.0 77.0 82.0 89.0 96.0 77.0 82.0 89.0 96.0	R.P.M. 775 778 781 785 790 795 800 805 810 9 R.P.M. 710 712 720	8.H.P. 58.0 65.0 68.0 74.0 79.0 91.0 99.0 106 " B.H.P. 69.0 76.0 83.0
		17000 18500 20000 21500 23500 24500 24500 27500 29000 29000 CapscRy in 20000 22000 24000 24000 25000 25000 26000 26000 26000	2860 3110 3370 3620 3870 4125 4370 4625 4880 Inlet Velocity F.P.M. 2830 3110 3400 3960 4250	400 405 410 430 445 460 475 490 510 2 2 R.P.M. 362 375 388 400 410 425	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0 *** B.H.P. 16.0 21.0 24.0	470 475 482 490 500 512 525 537 550 3 R.P.M. 425 435	21.0 23.0 26.0 29.0 33.0 37.0 41.0 46.0 51.0	R.P.M. 530 535 540 550 558 568 575 587 600 4R.P.M. 485 490 500	B.H.P. 27.0 29.0 33.0 36.0 44.0 48.0 54.0 59.0 TOTAL # B.H.P. 31.0 35.0 39.0	R.P.M. 590 595 600 605 610 615 625 635 640 PRESSU 540 545 550	33.0 36.0 39.0 43.0 47.0 52.0 57.0 68.0 RE OF : " B.H.P. 38.0 43.0	640 644 648 652 656 662 668 678 688 678 688 678 587 597 592 596	38.0 42.0 46.0 50.0 55.0 60.0 66.0 72.0 77.0 INCHES 77 8.H.P. 45.0 51.0 56.0	690 694 697 700 705 710 715 720 728 W. G. 7 R.P.M. 630 635 640	45.0 49.0 53.0 58.0 64.0 69.0 80.0 86.0 88.H.P. 54.0 65.0	R.P.M. 735 739 743 747 750 753 756 762 768 R.P.M. 675 675 680	8.H.P. 51.0 56.0 60.0 66.0 72.0 77.0 82.0 89.0 96.0	R.P.M. 775 778 781 785 790 795 800 805 810 9 R.P.M. 710 712 720	8.H.P. 58.0 65.0 68.0 74.0 79.0 85.0 91.0 99.0 106 8.H.P. 69.0 76.0 83.0
		17000 18500 20000 21500 23000 24500 24500 29000 Capscily in in C.FE. 20000 24000 24000 24000 28000 30000	2860 3110 3370 3620 3870 4125 4370 4625 4880 Iniet Velocity F.P.M. 2830 3110 3400 3680 3960 4250 4525	400 405 410 430 445 460 475 490 510: 2 R.P.M. 362 375 388 400 410 425 440	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0 21.0 24.0 27.0 32.0 38.0	470 475 482 490 500 512 525 537 550 3 R.P.M. 425 435 440 450 462 475	21.0 23.0 26.0 29.0 33,0 37.0 41.0 46.0 51.0 8.H.P. 24.0 28.0 32.0 36.0 41.0	R.P.M. 530 535 540 558 558 568 575 587 600 485 490 500 508 515 525	B.H.P. 27.0 29.0 33.0 40.0 44.0 48.0 54.0 59.0 TOTAL " B.H.P. 31.0 35.0 39.0 45.0 56.0 63.0	R.P.M. 590 595 600 615 625 635 640 PRESSU 540 545 550 555 568	33.0 36.0 39.0 43.0 47.0 52.0 57.0 63.0 68.0 RE OF : " B.H.P. 38.0 43.0 43.0 45.0 53.0 66.0 73.0	640 644 648 652 656 662 668 678 688 57STEM-6 7592 596 600 601 610	38.0 42.0 46.0 55.0 60.0 66.0 72.0 77.0 77.0 51.0 56.0 68.0 68.0 75.0	690 694 697 700 705 710 715 720 728 W. G. 728 630 635 640 645 650 655	45.0 49.0 53.0 58.0 64.0 69.0 74.0 80.0 86.0 86.0 72.0 78.0 65.0 72.0 78.0 94.0	R.P.M. 735 739 743 747 750 753 756 762 768 8R.P.M. 675 675 680 685 690 695 700	8.H.P. 51.0 56.0 66.0 72.0 77.0 82.0 89.0 96.0	R.P.M. 775 778 781 785 790 795 800 805 810 9 R.P.M. 710 712 720 725 730 735	8.H.P. 58.0 65.0 65.0 74.0 79.0 85.0 91.0 99.0 106 8.H.P. 69.0 76.0 83.0 90.0 98.0 106
		17000 18500 20000 21500 23500 24500 24500 27500 29000 29000 CapscRy in 20000 22000 24000 24000 25000 25000 26000 26000 26000	2860 3110 3370 3620 3870 4125 4370 4625 4880 Inlet Velocity F.P.M. 2830 3110 3400 3960 4250	400 405 410 430 445 460 475 490 510 2 2 R.P.M. 362 375 388 400 410 425	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0 21.0 24.0 27.0 32.0 38.0 45.0 50.0	470 475 482 490 512 525 537 550 3 R.P.M. 425 440 450 462 475 490 505	21.0 23.0 26.0 29.0 33.0 37.0 41.0 46.0 51.0 32.0 36.0 41.0 46.0 32.0 36.0 41.0 46.0	R.P.M. 530 535 540 558 558 575 587 600 48.P.M. 485 490 500 508 515 525 .	B.H.P. 27.0 29.0 33.0 40.0 44.0 48.0 54.0 59.0 TOTAL " B.H.P. 31.0 35.0 39.0 45.0 63.0 70.0	R.P.M. 590 595 600 615 625 635 640 PRESSU 540 545 550 555 560 5587	33.0 36.0 39.0 47.0 57.0 63.0 68.0 8E OF 5 8.H.P. 38.0 48.0 53.0 59.0 66.0 80.0	640 644 648 652 656 662 668 678 688 SYSTEM 6 7587 592 596 600 601 617 625	38.0 42.0 44.0 50.0 55.0 66.0 72.0 77.0 INCHES 7 8.H.P. 45.0 56.0 62.0 68.0 75.0 90.0	690 694 697 700 705 710 715 720 728 W. G. 7 8.P.M. 635 640 645 650 665	45.0 49.0 53.0 58.0 64.0 80.0 86.0 86.0 72.0 78.0 86.0 94.0 103	R.P.M. 735 739 743 747 750 753 756 762 768 8 R.P.M. 675 680 685 690 695 700 705	8.H.P. 51.0 56.0 60.0 66.0 72.0 77.0 82.0 89.0 96.0 7 8.H.P. 61.0 67.0 74.0 81.0 88.0 96.0	R.P.M. 775 778 781 785 790 795 800 805 810 9 R.P.M. 710 712 720 725 730 740 745	8.H.P. 58.0 65.0 68.0 74.0 91.0 91.0 99.0 106 83.0 90.0 98.0 106 115 125
		17000 18500 20000 21500 23000 24500 24500 29000 Capschy in C.F.fl. 20000 24000 24000 24000 28000 32000 34000	2860 3110 3370 3620 3870 4125 4370 4625 4880 Inlet Velocity F.P.M. 2830 3110 3400 3680 3960 4250 4525 4820	400 405 410 430 445 460 475 490 510: 2 R.P.M. 362 375 388 400 410 425 440 465	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0 21.0 24.0 27.0 32.0 38.0	470 475 482 490 500 512 525 537 550 3 R.P.M. 425 435 440 450 462 475	21.0 23.0 26.0 29.0 33,0 37.0 41.0 46.0 51.0 8.H.P. 24.0 28.0 32.0 36.0 41.0	R.P.M. 530 535 540 558 558 568 575 587 600 485 490 500 508 515 525	B.H.P. 27.0 29.0 33.0 40.0 44.0 48.0 59.0 TOTAL "B.H.P. 31.0 35.0 39.0 45.0 63.0 70.0	R.P.M. 590 595 600 605 610 615 625 635 540 540 545 550 555 560 568 577 587	33.0 36.0 39.0 47.0 52.0 57.0 63.0 68.0 73.0 43.0 48.0 59.0 59.0 66.0 73.0 88.0 88.0	640 644 648 655 662 668 678 688 578 587 592 596 600 610 617 625 635	38.0 42.0 44.0 50.0 55.0 66.0 72.0 77.0 77.0 51.0 56.0 68.0 68.0 68.0 90.0 99.0	690 694 697 700 705 710 715 720 728 W. G. 82.P.M. 635 640 645 655 660 665 675	45.0 49.0 53.0 58.0 64.0 69.0 74.0 80.0 86.0 86.0 72.0 78.0 65.0 72.0 78.0 94.0	R.P.M. 735 739 743 747 750 753 756 762 768 8R.P.M. 675 675 680 685 690 695 700	8.H.P. 51.0 56.0 66.0 72.0 77.0 82.0 89.0 96.0	R.P.M. 775 778 781 785 790 795 800 805 810 9 R.P.M. 710 712 720 725 730 735	8.H.P. 58.0 65.0 65.0 74.0 79.0 85.0 91.0 99.0 106 8.H.P. 69.0 76.0 83.0 90.0 98.0 106
		17000 18500 20000 21500 23500 24500 24500 25500 29000 29000 20000 22000 24000 26000 28000 30000 32000 34000 36000	2860 3110 3370 3620 3870 4125 4370 4625 4880 Inlet Velocity F.P.M. 2830 3110 3400 3680 3960 4250 4525 4820 5100	2 R.P.M. 362 375 388 400 410 425 440 465 480	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0 21.0 24.0 27.0 32.0 38.0 45.0 50.0 55.0	470 475 482 490 500 512 525 537 550 3 R.P.M. 425 435 440 450 462 475 490 505 520	21.0 23.0 26.0 29.0 33,0 37.0 41.0 46.0 51.0 28.0 32.0 36.0 41.0 46.0 53.0 60.0 68.0	R.P.M. 530 535 540 550 558 568 575 587 600 48.P.M. 485 490 500 500 505 515 525 535 550 565	B.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 59.0 TOTAL ** B.H.P. 31.0 35.0 39.0 45.0 56.0 63.0 77.0 TOTAL	R.P.M. 590 595 600 615 625 635 640 PRESSU 540 545 550 555 560 568 577 587 600	33.0 36.0 39.0 47.0 52.0 57.0 63.0 68.0 RE OF 1 8.H.P. 38.0 43.0 48.0 73.0 59.0 66.0 73.0 80.0 88.0	640 644 648 655 6662 668 678 688 578TEM-6 7592 596 600 601 617 625 635	38.0 42.0 46.0 50.0 55.0 66.0 72.0 77.0 71.0 51.0 56.0 68.0 90.0 99.0	690 694 697 700 705 710 715 720 728 W. G. 7 R.P.M. 630 635 640 645 650 665 660 665 675	45.0 49.0 53.0 58.0 64.0 69.0 74.0 80.0 86.0 72.0 78.0 65.0 72.0 78.0 94.0	R.P.M. 735 739 747 750 753 756 768 8R.P.M. 675 675 680 685 690 695 700 705 710	8.H.P. 51.0 56.0 66.0 66.0 72.0 77.0 82.0 89.0 96.0 78.H.P. 61.0 67.0 74.0 81.0 88.0 96.0 105 113 123	R.P.M. 775 778 781 785 790 795 800 805 810 9 R.P.M. 710 712 720 725 730 745 750	8.H.P. 58.0 65.0 65.0 74.0 77.0 85.0 91.0 99.0 106 8.H.P. 69.0 76.0 83.0 90.0 98.0 106 115 125
		17000 18500 20000 21500 23000 24500 26000 27500 29000 25.56 20000 24000 24000 24000 25000 28000 30000 30000 34000 36000	2860 3110 3370 3620 3870 4125 4370 4625 4880 Inlet Velocity F.P.M. 2830 3110 3400 3400 3960 4250 4525 4820 5100	400 405 410 430 445 460 475 490 510: 2 R.P.M. 362 375 388 400 410 425 440 465 480	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0 21.0 24.0 27.0 32.0 45.0 50.0 55.0	470 475 482 490 510 512 525 537 550 3 R.P.M. 425 435 440 450 462 475 490 505 520	21.0 23.0 26.0 29.0 33.0 37.0 41.0 46.0 51.0 28.0 32.0 36.0 41.0 46.0 53.0 60.0 68.0	R.P.M. 530 535 540 558 558 575 587 600 48.P.M. 485 490 500 508 515 525 .	B.H.P. 27.0 29.0 33.0 40.0 44.0 48.0 59.0 TOTAL 7 50.0 63.0 70.0 77.0 TOTAL	R.P.M. 590 595 600 605 610 615 625 636 640 PRESSU 540 545 550 555 560 568 577 587 600	33.0 36.0 39.0 47.0 57.0 63.0 68.0 88.0 88.0 88.0 88.0	640 644 648 652 656 662 668 678 688 SYSTEM 6 7587 592 596 600 601 617 625 635	38.0 42.0 44.0 50.0 55.0 66.0 72.0 77.0 -INCHES 7 8.H.P. 45.0 62.0 68.0 75.0 90.0 99.0	690 694 697 700 705 710 715 720 728 W. G. 7 R.P.M. 635 640 645 650 665 660 665 675 W. G.	45.0 49.0 53.0 58.0 64.0 69.0 74.0 80.0 86.0 72.0 72.0 72.0 78.0 94.0 103 111	R.P.M. 735 739 743 747 750 753 756 762 768 8.P.M. 675 675 680 685 690 695 700 705 710	8.H.P. 51.0 56.0 66.0 72.0 77.0 82.0 89.0 96.0 7 8.H.P. 61.0 67.0 74.0 88.0 96.0 105 113 123	R.P.M. 775 778 781 785 790 795 800 805 810 9 R.P.M. 710 712 720 725 730 745 750	8.H.P. 58.0 65.0 65.0 74.0 79.0 85.0 91.0 99.0 106 8.H.P. 69.0 76.0 83.0 90.0 98.0 105 115 125 136
		17000 18500 20000 21500 23500 24500 24500 25500 29000 Capselly in C.F.fil. 20000 24000 24000 24000 30000 30000 34000 34000 36000 Capselly in C.F.M. 32500	2860 3110 3370 3620 3870 4125 4370 4625 4880 Inlet Velocity F.P.M. 2830 3400 3400 3480 3960 4250 4525 4820 5100	2 R.P.M. 362 375 388 400 410 425 440 465 480	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0 21.0 24.0 27.0 32.0 38.0 45.0 50.0 55.0	470 475 482 490 500 512 525 537 550 3 R.P.M. 425 435 440 450 462 475 490 505 520	21.0 23.0 26.0 29.0 33.0 37.0 41.0 46.0 51.0 32.0 36.0 41.0 46.0 53.0 60.0 68.0	R.P.M. 530 535 540 558 558 568 575 587 600 48.P.M. 485 490 500 508 515 525 535 550 565	B.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 59.0 TOTAL ** B.H.P. 31.0 35.0 39.0 45.0 56.0 63.0 77.0 TOTAL	R.P.M. 590 595 600 615 625 635 640 PRESSU 540 545 550 555 560 568 577 587 600	33.0 36.0 39.0 47.0 52.0 57.0 63.0 68.0 RE OF 1 8.H.P. 38.0 43.0 48.0 73.0 59.0 66.0 73.0 80.0 88.0	640 644 648 655 6662 668 678 688 578TEM-6 7592 596 600 601 617 625 635	38.0 42.0 46.0 50.0 55.0 66.0 72.0 77.0 71.0 51.0 56.0 68.0 90.0 99.0	690 694 697 700 705 710 715 720 728 W. G. 7 R.P.M. 630 635 640 645 650 665 660 665 675	45.0 49.0 53.0 58.0 64.0 69.0 74.0 80.0 86.0 72.0 78.0 65.0 72.0 78.0 94.0	R.P.M. 735 739 747 750 753 756 768 8R.P.M. 675 675 680 685 690 695 700 705 710	8.H.P. 51.0 56.0 66.0 66.0 72.0 77.0 82.0 89.0 96.0 78.H.P. 61.0 67.0 74.0 81.0 88.0 96.0 105 113 123	R.P.M. 775 778 781 785 790 795 800 805 810 9 R.P.M. 710 712 720 725 730 745 750	8.H.P. 58.0 65.0 65.0 74.0 77.0 85.0 91.0 99.0 106 8.H.P. 69.0 76.0 83.0 90.0 98.0 106 115 125
		17000 18500 20000 21500 23500 24500 24500 25500 29000 CapscRy in 20000 22000 24000 25000 30000 30000 32000 34000 34000 CapscRy in 32500 35000	2860 3110 3370 3620 3870 4125 4370 4625 4880 Inlet Velocity F.P.M. 2830 3110 3400 3580 4250 4525 4820 5100 Inlet Velocity F.P.M. 2940 3170	20 445 460 475 490 510 438 400 425 440 445 480 22 R.P.M. 290 300	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0 21.0 24.0 27.0 32.0 38.0 45.0 55.0	470 475 482 490 500 512 525 537 550 3 R.P.M. 425 435 440 450 450 450 505 520 3 R.P.M. 345 490 505 520	21.0 23.0 26.0 29.0 33.0 37.0 41.0 46.0 51.0 8.H.P. 24.0 28.0 32.0 36.0 46.0 68.0	R.P.M. 530 535 540 550 558 568 575 587 600 485 490 508 515 525 535 550 565	B.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 59.0 TOTAL B.H.P. 31.0 35.0 39.0 56.0 63.0 77.0 TOTAL B.H.P. 59.0 56.0 55.0	R.P.M. 590 595 600 605 610 615 625 636 640 PRESSUI 540 545 550 568 577 587 600 PRESSUI 5 8 7 8 8 8 9 9 9 9 9 9 9 9 9 9 9 9 9	33.0 36.0 39.0 47.0 52.0 57.0 63.0 68.0 7 8.H.P. 38.0 43.0 48.0 59.0 66.0 73.0 80.0 88.0 88.0	640 644 648 655 656 662 668 678 688 578 587 592 596 600 610 617 625 635 75TEM-6 67.7 67.7 67.7 67.7 67.7 67.7 67.7 67	38.0 42.0 44.0 50.0 55.0 60.0 66.0 77.0 77.0 1NCHES 77.0 51.0 56.0 62.0 68.0 75.0 83.0 90.0 99.0 99.0 99.0	690 694 697 700 705 710 715 728 W. G. 728 630 635 640 645 650 655 660 665 675 W. G.	### ### ### ### ### ### ### ### ### ##	R.P.M. 735 739 743 747 750 753 756 762 768 8.P.M. 675 675 680 685 690 695 700 705 710 8.P.M. 540 540	8.H.P. 51.0 56.0 66.0 66.0 72.0 77.0 82.0 89.0 96.0 8.H.P. 61.0 67.0 74.0 88.0 96.0 105 113 123	R.P.M. 775 778 781 785 790 795 800 805 810 710 712 720 725 730 735 740 745 750 9 R.P.M.	8.H.P. 58.0 65.0 65.0 74.0 79.0 85.0 91.0 99.0 106 " B.H.P. 69.0 76.0 83.0 90.0 90.0 90.0 115 125 136
		17000 18500 20000 21500 23500 24500 24500 25500 29000 Capselly in 20000 24000 24000 24000 34000 34000 36000 Capselly in C.F.M. 32500 37500	2860 3110 3370 3620 3870 4125 4370 4625 4880 Inlet Velocity F.P.M. 2830 3110 3400 3680 3960 4250 4525 4820 5100 Inlet Velocity F.P.M.	2 R.P.M. 400 405 410 430 445 460 510 10 10 10 10 10 10 10 10 10 10 10 10 1	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0 21.0 24.0 27.0 32.0 38.0 45.0 55.0	370 475 482 490 500 512 525 537 550 3 R.P.M. 425 435 440 450 462 475 490 505 520 3 R.P.M. 345 345 345 345 345 345 345 345 345	21.0 23.0 26.0 29.0 33,0 37.0 41.0 46.0 51.0 28.0 32.0 36.0 41.0 46.0 53.0 60.0 68.0	R.P.M. 530 535 540 550 558 568 575 587 600 48.P.M. 485 490 500 505 515 525 535 550 565	B.H.P. 27.0 29.0 33.0 40.0 44.0 48.0 59.0 TOTAL 31.0 35.0 39.0 45.0 70.0 77.0 TOTAL 7 B.H.P. 59.0 55.0 62.0 62.0	R.P.M. 590 595 600 615 625 636 640 PRESSUI 540 545 550 568 577 587 600 PRESSUI 430 435 440	33.0 36.0 39.0 47.0 52.0 57.0 63.0 68.0 88.0 43.0 43.0 48.0 73.0 80.0 88.0 88.0 88.0 88.0 88.0	640 644 648 652 656 662 668 678 688 578 587 592 596 600 601 617 625 635 678 678 678 678 678 678 678 678 678 678	38.0 42.0 44.0 50.0 55.0 66.0 72.0 77.0 77.0 51.0 56.0 68.0 90.0 99.0 99.0 1NCHES "" B.H.P. 75.0 83.0 99.0 99.0	690 694 697 700 705 710 715 720 728 W. G. 7 R.P.M. 635 640 645 650 665 660 665 675 W. G. 7 R.P.M. 510 511 511 515	45.0 49.0 53.0 58.0 64.0 69.0 74.0 80.0 86.0 72.0 78.0 65.0 72.0 78.0 94.0 103 111	R.P.M. 735 739 743 747 750 753 756 768 8 R.P.M. 675 675 680 695 700 705 710 8 R.P.M. 540 540 545	8.H.P. 51.0 56.0 66.0 66.0 72.0 77.0 82.0 89.0 96.0 78.H.P. 61.0 67.0 74.0 81.0 96.0 105 113 123	R.P.M. 775 778 781 785 790 795 800 805 810 9 R.P.M. 710 712 720 725 730 735 740 745 750	8.H.P. 58.0 65.0 65.0 74.0 79.0 85.0 91.0 99.0 106 76.0 83.0 90.0 106 115 125 136
		17000 18500 20000 21500 23500 24500 24500 25500 29000 CapscRy in 20000 22000 24000 25000 30000 30000 32000 34000 34000 CapscRy in 32500 35000	2860 3110 3370 3620 3870 4125 4370 4625 4880 Inlet Velocity F.P.M. 2830 3110 3400 3580 4250 4525 4820 5100 Inlet Velocity F.P.M. 2940 3170	20 445 460 475 490 510 438 400 425 440 445 480 22 R.P.M. 290 300	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0 21.0 24.0 27.0 32.0 38.0 45.0 55.0	470 475 482 490 500 512 525 537 550 3 R.P.M. 425 435 440 450 450 450 505 520 3 R.P.M. 345 490 505 520	21.0 23.0 26.0 29.0 33.0 37.0 41.0 46.0 51.0 8.H.P. 24.0 28.0 32.0 36.0 46.0 68.0	R.P.M. 530 535 540 550 558 568 575 587 600 485 490 508 515 525 535 550 565	B.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 59.0 TOTAL B.H.P. 31.0 35.0 39.0 56.0 63.0 77.0 TOTAL B.H.P. 59.0 56.0 55.0	R.P.M. 590 595 600 605 610 615 625 636 640 PRESSUI 540 545 550 568 577 587 600 PRESSUI 5 8 7 8 8 8 9 9 9 9 9 9 9 9 9 9 9 9 9	33.0 36.0 39.0 47.0 52.0 57.0 63.0 68.0 7 8.H.P. 38.0 43.0 48.0 59.0 66.0 73.0 80.0 88.0 88.0	640 644 648 652 656 662 668 678 688 SYSTEM 6 7 592 596 600 601 617 625 635 F.P.M. 470 470 470 470 485	38.0 42.0 44.0 50.0 55.0 60.0 66.0 77.0 77.0 -INCHES 7 8.H.P. 45.0 62.0 62.0 68.0 90.0 99.0 99.0	690 694 697 700 715 710 715 720 728 W. G. 7 R.P.M. 635 640 645 650 665 660 665 675 W. G. 7 R.P.M. 510 512 515 517	## ## ## ## ## ## ## ## ## ## ## ## ##	R.P.M. 735 739 743 747 750 753 756 762 768 8.P.M. 675 675 680 685 690 695 700 705 710 8.P.M. 540 540	8.H.P. 51.0 56.0 66.0 72.0 77.0 82.0 89.0 96.0 67.0 74.0 81.0 88.0 96.0 105 113 123	R.P.M. 775 778 781 785 790 795 800 805 810 9 R.P.M. 710 712 720 725 730 745 750 9 R.P.M. 570 573 575 578	8.H.P. 58.0 65.0 65.0 74.0 79.0 85.0 91.0 99.0 106 " B.H.P. 69.0 76.0 83.0 90.0 90.0 90.0 115 125 136
		17000 18500 20000 21500 225000 24500 24500 229000 229000 22000 22000 24000 22000 24000 30000 30000 32000 34000 34000 Capacity In	2860 3110 3370 3620 3870 4125 4370 4625 4880 hilet Velocity F.P.M. 2830 3110 3400 3400 3960 4250 5100 hilet Velocity F.P.M. 2830 3960 4250 5100 hilet Velocity F.P.M. 3170 3480 3960 4250 5100 5100 5100 5100 5100 5100 5100 5	2 R.P.M. 250 480 485 480 275 480 315 315	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0 21.0 24.0 27.0 32.0 50.0 55.0	470 475 482 490 510 512 525 537 550 3 R.P.M. 435 440 450 462 475 490 505 520 3 R.P.M. 345 350 355 365	21.0 23.0 26.0 29.0 33,0 37.0 41.0 46.0 51.0 28.0 32.0 36.0 41.0 46.0 53.0 60.0 68.0	R.P.M. 530 535 540 550 558 568 575 587 600 48.P.M. 485 490 508 515 525 535 550 565 4.R.P.M. 390 395 400 405 410 415	B.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 55.0 70.0 55.0 63.0 77.0 77.0 55.0 62.0 68.0 74.0 81.0	R.P.M. 590 595 600 605 610 615 625 635 640 PRESSUI 540 545 550 568 577 587 600 PRESSUI 430 435 440 445 450 455	33.0 36.0 39.0 47.0 52.0 57.0 63.0 68.0 88.0 88.0 73.0 80.0 88.0 88.0 88.0 88.0 88.0 88.0 8	640 644 648 652 656 662 668 678 688 578 587 592 596 600 601 617 625 635 678 678 678 678 678 678 678 678 678 678	38.0 42.0 44.0 50.0 55.0 66.0 72.0 77.0 77.0 51.0 56.0 68.0 90.0 99.0 99.0 1NCHES "" B.H.P. 75.0 83.0 99.0 99.0	690 694 697 700 705 710 715 720 728 W. G. 7 R.P.M. 635 640 645 650 665 660 665 675 W. G. 7 R.P.M. 510 511 511 515	45.0 49.0 53.0 58.0 64.0 69.0 74.0 80.0 86.0 72.0 78.0 65.0 72.0 78.0 94.0 103 111	R.P.M. 735 739 743 747 750 753 756 762 768 R.P.M. 675 675 680 685 690 695 700 705 710 8 R.P.M. 540 540 545 548	8.H.P. 51.0 56.0 66.0 66.0 72.0 77.0 82.0 89.0 96.0 78.H.P. 61.0 67.0 74.0 81.0 96.0 105 113 123	R.P.M. 775 778 781 785 790 795 800 805 810 9 R.P.M. 710 712 720 725 730 735 740 745 750	8.H.P. 58.0 65.0 65.0 74.0 77.0 85.0 91.0 99.0 106 83.0 90.0 98.0 115 125 136 8.H.P. 112 120 130
		17000 18500 20000 21500 225000 24500 24500 229000 229000 22000 24000 22000 24000 30000 32000 34000 34000 35000 37500 37500 40000 425000 425000 425000 425000	2860 3110 3370 3620 3870 4125 4370 4625 4880 Inlet Velocity F.P.M. 2830 3110 3400 3580 3960 4250 4525 4820 5100 Inlet Velocity F.P.M. 2940 3170 3390 3620 3850 3850 3950 4075 4300	20 445 460 475 490 510 410 425 440 445 480 20 310 315 325 345	15.0 17.0 20.0 23.0 26.0 29.0 34.0 39.0 44.0 21.0 24.0 27.0 32.0 38.0 45.0 55.0 55.0 43.0 48.0 48.0 48.0 55.0 62.0	370 475 482 490 500 512 525 537 550 3 R.P.M. 425 435 440 450 450 450 450 450 450 450 450 45	21.0 23.0 26.0 29.0 33.0 37.0 41.0 46.0 51.0 8.H.P. 24.0 28.0 32.0 36.0 46.0 53.0 60.0 68.0	R.P.M. 530 535 540 550 558 568 575 600 48.P.M. 485 490 500 508 515 525 535 550 565 400 405 415 420	B.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 59.0 70TAL 70TAL 70 8.H.P. 31.0 35.0 39.0 63.0 77.0 TOTAL 70TAL	R.P.M. 590 595 600 605 610 615 625 635 640 PRESSUI 540 545 550 568 577 587 600 PRESSUI 540 435 440 445 4450 4455 460	33.0 36.0 39.0 47.0 52.0 57.0 63.0 68.0 73.0 43.0 43.0 48.0 73.0 80.0 88.0 88.0 88.0 88.0 88.0 88.0 8	640 644 648 655 662 668 678 688 FR.P.M. 587 592 596 600 610 617 625 635 FR.P.M. 470 475 480 488 490	38.0 42.0 44.0 50.0 55.0 66.0 77.0 77.0 77.0 51.0 51.0 56.0 68.0 68.0 99.0 99.0 INCHES " B.H.P. 75.0 88.0 95.0 103 110	690 694 697 700 705 710 715 720 728 W. G. 635 640 645 655 660 655 660 665 675 W. G. 7 R.P.M. 510 512 515 517 520 523 525	### ### ### ### ### ### ### ### ### ##	R.P.M. 735 739 743 747 750 753 756 762 768 R.P.M. 675 675 680 685 690 695 700 705 710 R.P.M. 540 545 548 550 552	8.H.P. 51.0 56.0 66.0 66.0 72.0 77.0 82.0 89.0 96.0 8.H.P. 61.0 67.0 74.0 88.0 96.0 105 113 123 8.H.P. 100 108 115 123	R.P.M. 775 778 781 785 780 795 800 805 810 712 710 712 720 725 730 735 740 745 750 9 R.P.M. 570 573 575 578 582 585	8.H.P. 58.0 65.0 65.0 74.0 79.0 85.0 91.0 99.0 106 " B.H.P. 69.0 76.0 83.0 90.0 98.0 106 115 125 136 " B.H.P. 112 120 130 138 158 168
		17000 18500 20000 21500 225000 24500 24500 229000 229000 22000 22000 24000 22000 24000 30000 30000 32000 34000 34000 Capacity In	2860 3110 3370 3620 3870 4125 4370 4625 4880 hilet Velocity F.P.M. 2830 3110 3400 3400 3960 4250 5100 hilet Velocity F.P.M. 2830 3960 4250 5100 hilet Velocity F.P.M. 3170 3480 3960 4250 5100 5100 5100 5100 5100 5100 5100 5	20 445 440 445 440 445 440 445 440 445 440 445 480 27 R.P.M. 290 300 310 315 325 335	15.0 17.0 20.0 23.0 24.0 39.0 44.0 39.0 44.0 21.0 24.0 32.0 38.0 45.0 55.0	470 475 482 490 500 512 525 537 550 3 R.P.M. 425 435 440 450 450 462 475 490 505 520 3 R.P.M. 345 350 355 350 355 370 375	21.0 23.0 26.0 29.0 33.0 37.0 41.0 46.0 51.0 28.0 32.0 46.0 41.0 46.0 53.0 60.0 44.0 48.0 44.0 48.0 54.0 60.0 67.0	R.P.M. 530 535 540 550 558 568 575 587 600 48.P.M. 485 490 508 515 525 535 550 565 4.R.P.M. 390 395 400 405 410 415	B.H.P. 27.0 29.0 33.0 36.0 40.0 44.0 48.0 55.0 70.0 55.0 63.0 77.0 77.0 55.0 62.0 68.0 74.0 81.0	R.P.M. 590 595 600 605 610 615 625 635 640 PRESSUI 540 545 550 568 577 587 600 PRESSUI 430 435 440 445 450 455	33.0 36.0 39.0 47.0 47.0 52.0 57.0 63.0 68.0 78.0 43.0 48.0 53.0 66.0 73.0 80.0 88.0 88.0 88.0 75.0 68.0 75.0 68.0 75.0	640 644 648 655 666 662 668 678 688 578 587 592 596 600 617 625 600 617 625 635 775TEM 670 475 480 488 490	38.0 42.0 44.0 50.0 55.0 60.0 66.0 77.0 77.0 45.0 51.0 56.0 62.0 68.0 75.0 83.0 99.0 99.0 1NCHES 75.0 88.0 99.0	690 694 697 700 705 710 715 728 W. G. 7 R.P.M. 630 635 640 645 650 655 660 655 675 W. G. 7 R.P.M. 510 512 515 517 520 523	## ## ## ## ## ## ## ## ## ## ## ## ##	R.P.M. 735 739 743 747 750 753 756 762 768 8 R.P.M. 675 675 680 685 690 695 700 705 710 8 R.P.M. 540 540 545 548 550 552	8.H.P. 51.0 56.0 60.0 72.0 77.0 82.0 89.0 96.0 8.H.P. 61.0 67.0 74.0 88.0 96.0 105 113 123	R.P.M. 775 778 781 785 790 795 800 805 810 712 720 712 720 735 740 745 750 9 R.P.M. 570 573 575 578	8.H.P. 58.0 65.0 65.0 74.0 79.0 85.0 91.0 99.0 106 83.0 90.0 98.0 106 115 125 136 8.H.P. 112 120 130 138 148 158

ROTO-CLONE ERECTION DIAGRAM Arrangements A and D

Type W Spray Nozzle Connection

Rubber Gasket Arrangement D Inlet Transition



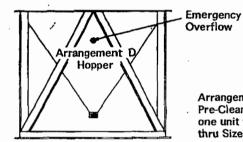
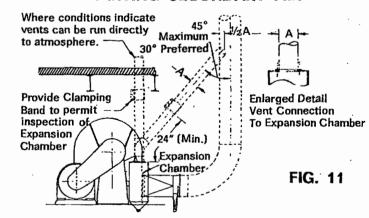


FIG. 10

Arrangement D Hopper and Pre-Cleaner shipped as one unit for Roto-Clones thru Size No. 20.

VENTING SECONDARY AIR



DIMENSION TABLE IN INCHES

R. C. Size	8	10	12	14	16	20	24	27	30	33	36	45
Vent Dia. "A"	31/2"	4"	5"	6″	7"	8″	10″	11"	12"	14"	15″	18"

TABLE A NORMAL WATER SUPPLY RATES TYPE W ROTO-CLONES

Roto-		rrang emeat GPM Supplie		Arrangement D GPM Supplied				
Size	40 PSIG	50 PSIG	60 PSIG	40 PSIG	50 PSIG	60 PSIG		
8	1.1	1.2	1.3	2.1	2.2	2.5		
10	1.5	1.6	1.8	3.1	3.4	3.8		
12	1.8	2.0	2.2	4.6	5.0	5.4		
14	2.3	2.5	2.9	5.1	5.5	6.3		
16	3.4	3.7	4.1	7.2	7.9	8.7		
20	4.4	4.8	5.4	8.2	9.0	10.0		
24	5.4	6.0	6.5	13.2	14.9	16.1		
27	7.4	8.2	8.9					
30	7.9	8.8	9.7		}	l ~		
33	11.9	13.3	14.6	l				
36	13.9	15.7	17,0		!			
45	20.9	25.1	25.2	!	l			

NOTE: 1: For air temperatures in excess of 300°F, cooling spray nozzles should be provided in inlet duct to compensate for evaporation. A safe approximation will be 0.2 gpm of additional water per 1000 cfm for each 100°F temperature reduction.

TABLE B SHIPPING AND OPERATING WEIGHTS

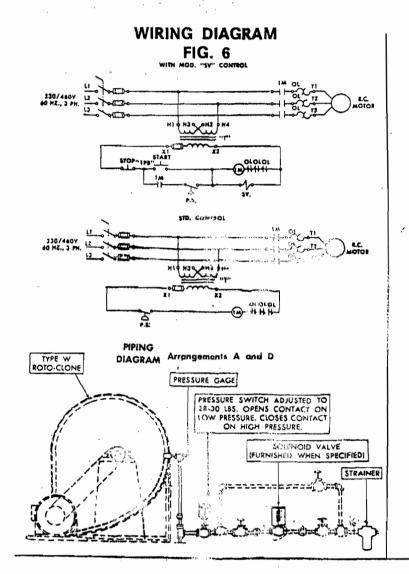
Roto-	Arrange	ement A	Arrong	Arrongement D			
Clone Size	Shipping Operating Weight (lbs.)		Shipping Weight (lbs.)	Operating Weight (lbs.)			
8	225	425	1,725	2,625			
10	360	610	1,810	3,010			
12	630	880	2,030	3,380			
14	990	1,340	2,790	5,320			
16	1,260	1,710	3,760	6,310			
20	1,620	2,270	5,420	9,650			
24	1,890	2,590	7,190	13,290			
. 27	2,970	3,720	_				
30	3,870	5,020		l —			
33	4,860	6,360					
36	5,850	7,350					
45	13,500	16,000					

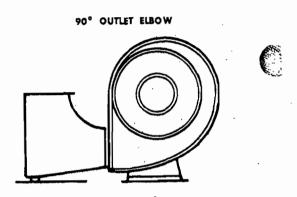
NOTE 1: Shipping weight does not include motor and drive.

NOTE 2: Operating weight includes motor and drive for Arrangements, "A" and "D". Also includes maximum sludge capacity based on 100 lbs. per cubic foot for Arrangement D hopper in the event of plugged drain line.

TABLE C TYPE W ROTO-CLONE IMPELLER CHARACTERISTICS

Rato-Clone Size	Maximum Speed (RPM)	Fly Wheel Effect - WR ² (Lb Ft. ²)		
8	4100			
10	3300	6.28		
12	2800	14.7		
14	2400	30.7		
16	2100	50.8		
20	1700	150.8		
24	1400	372.0		
27	1250	596.0		
30	1100	1026.0		
33	1000	1400.0		
36	925	2410.0		
45	730	6250.0		



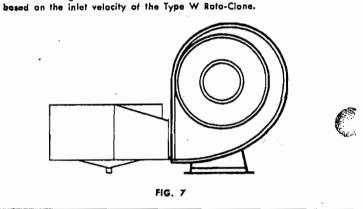


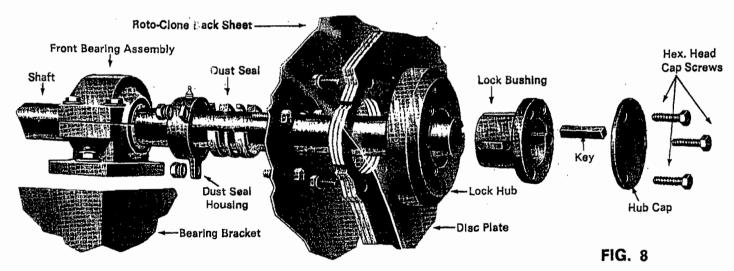
The 90° outlet elbow is recommended where a vertical stack is required immediately at the Roto-Clone discharge. Refer to Drawing 48P-870790 for dimensions.

FIG. 6 CENTRIFUGAL OUTLET

The centrifugal autiet is recommended where cleaned air is recirculated back to work area or where corresive mists may be exhausted. It protects against possible damage from occasional water droplets. The centrifugal outlet replaces and is interchangeable with the standard air outlet. Ask for Drawing 48P-1023266 showing dimensions of this accessory.

If the centrifugal outlet is used there is an additional loss of 2YP





SHAFT ASSEMBLY

Construction details of Type W Roto-Clone shaft assembly showing heavy duty bearings, oversized shaft, watertight, shaft seal, laminated impeller disc, and cast iron hub with taper lock for easy impeller removal.

6

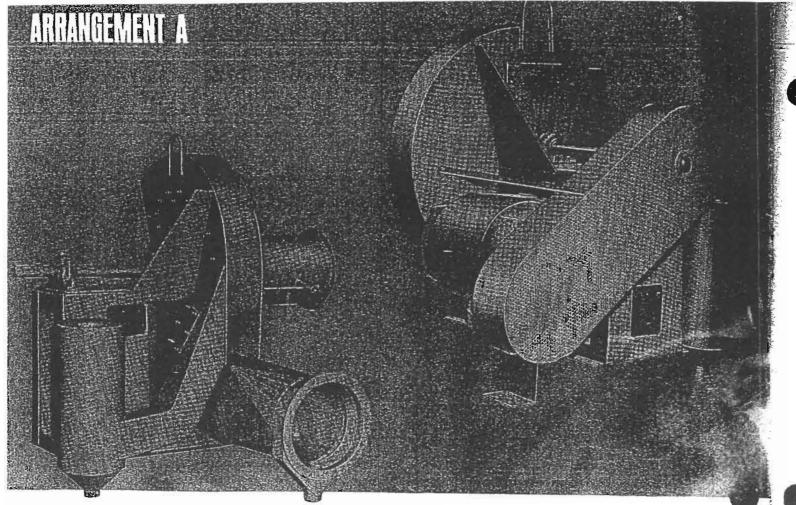


FIG. 2

Type W Roto-Clone, Arrangement A, from drive side. Clean air outlet may be horizontal duct, as shown, or rectangular elbow.

The Type W Roto-Clone, Arrangement A, is recommended for the collection of light loadings of granular dusts and mist. Dynamic forces developed by the rotating impeller cause even the finest particles to impinge on and be trapped by the flowing water film which covers all blade surfaces. The slurry formed by water and collected dust drains from the bottom of the Roto-Clone expansion chamber (see Figure 1). Slurry may be piped to a sump or sewer, returned to process, or discharged to a settling tank where the collected solids precipitate by gravity and clear water overflows to the sewer or drain.

The Type W Roto-Clone has the performance characteristics of a centrifugal fan. The relation between pressure, volume, and horsepower follows the standard laws of fan performance. Maximum operating speeds are shown in Table C, page 11.

If high temperature, corrosive, or toxic exhaust gases are cleaned, the expansion chamber should be vented to the outside of the building as illustrated in Figure 11, page 11.

FIG.

Type W Roto-Clone, Arrangement A, is available in Arrangement 9 motor mounting where dimensions permit mounting motor on bearing pedestal.

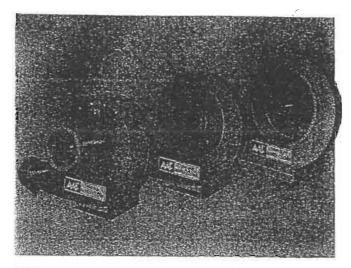
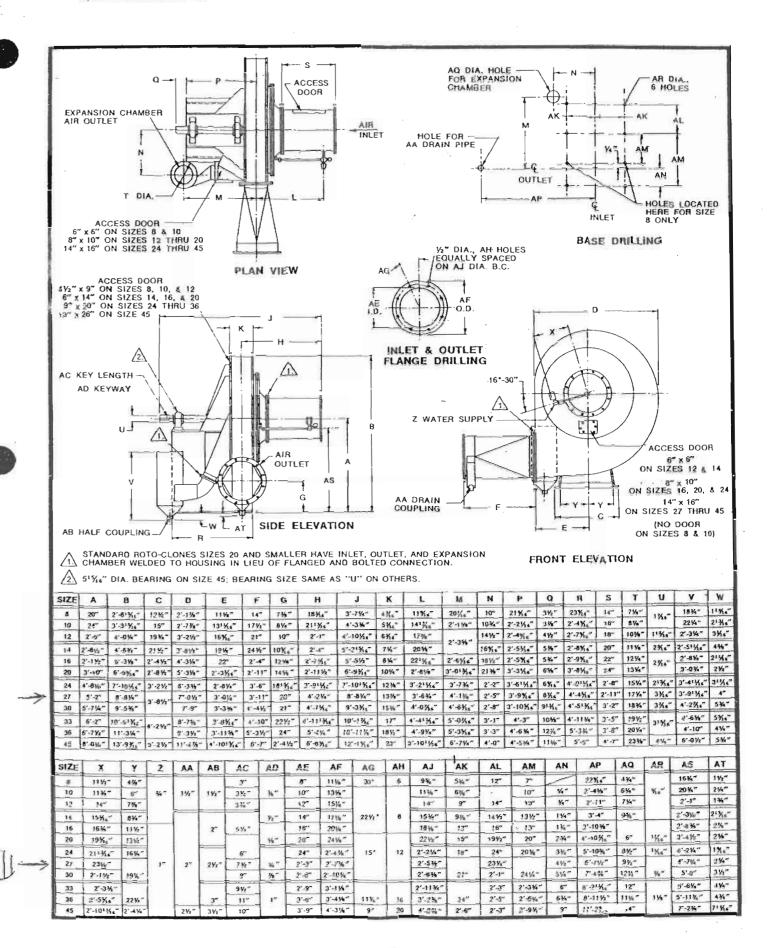


FIG. 4

Standard construction includes brass spray nozzles, stainless steel impeller blades and rivets. Water cone, impeller discs. and welded housing are hot rolled steel plate. All parts can be supplied of aluminum, stainless steel or other metals or the internal housing can be protected with corrosion resistant material (the impeller cannot be coated). See Fig. 5 for additional construction data.



COLLECTS MORE DUST FOR FEWER DOLLARS!

The Type W Roto-Clone has become a dust control favorite throughout industry. The reason: Type W is the lowest priced high efficiency wet dust collector in its class.

The distinguishing feature of the Type W is the addition of water sprays to the basic principle of dynamic precipitation. The spray maintains a flowing film of water on all collecting surfaces which:

- 1. Lowers water requirements to a minimum.
- 2. Traps even the lightest and finest dust particles.
- 3. Delivers collected dust in slurry form for easy disposal.

Type W Roto-Clone provides everything you need, except duct connections, in one complete, shop-assembled package — high efficiency collector, exhauster, motor and drive. Available in 12 sizes from 1,000 to 50,000 cfm.

For heavy dust concentrations, a Precleaner is used with the Type W. The Precleaner removes the bulk of the dust, either wet or dry, leaving only the fines to be collected by the Roto-Clone.

Highest Efficiency

Combines dynamic precipitation with a water spray. Maintains efficiency over entire operation range, regardless of speed or air volume. 98% or better dust removal for most applications.

Minimum Water Requirement

Water consumption is limited to a small amount required to maintain a flowing film on all collecting surfaces. From ½ to 1 gallon per 1,000 cfm of air cleaned.

Small Space Requirements

Roto-Clone combines exhauster and dust collector. Basically no larger than a centrifugal exhauster.

Low Installation Cost

Factory-assembled, tested, and shipped in sub-assemblies convenient to handle and easy to erect. As simple to install as a centrifugal fan with the exception that furnace type ducting is not recommended—use welded duct. Water supply and drain are the only additional connections.

Continuous Operation

Uniform performance at peak efficiency without interruption for reconditioning or servicing of any kind. Will operate around the clock — day after day.

Great Flexibility

Variety of sizes for any exhaust requirement. Compact design allows relocation at minimum expense. Sizes with capacities from 1,000 to 50,000 cfm.

Constant Exhaust Volume

Proper conveying velocity in ducts and effective dust control at hoods maintained by constant exhaust air voi; me. Build-up in ducts and escapement from hoods is prevented.

No Secondary Dust Problem

Collected dust discharges as slurry to process, sewer or sump.

OPERATING PRINCIPLE

The dust laden air enters the Type W Roto-Clone where it is subjected to a fine water spray. The water and dust being heavier than air impinge on the blades of the impeller and then are directed into the water cone by the special blade design and the centrifugal force of the rotating impeller. The slurry drains from the unit through the sludge chute to the expansion chamber.

The impeller imparts energy to the clean air which being lighter than the water and dust is discharged in front of the water cone and continues on to the clean air outlet.

Dust Laden Air

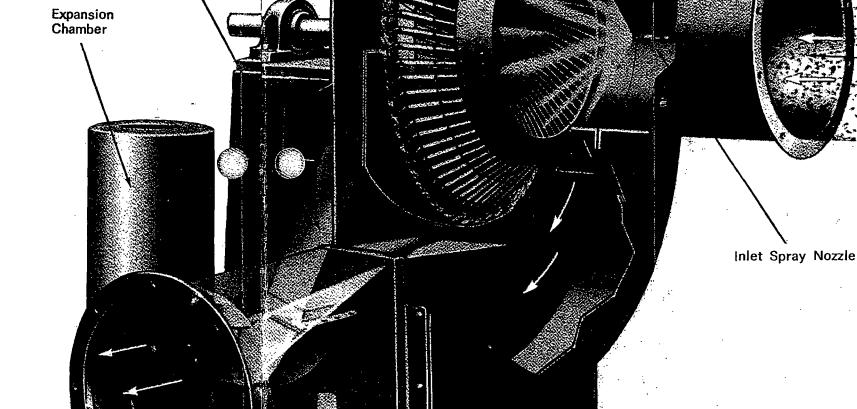


FIG. 1

Water Cone

Impeller

Sludge Chute

Capacity ratings and blower performance ______Pages 8-10

Special arrangements ______Page 6

Water requirements ______Page 11

Shipping and operating weights _____Page 11

2

Clean

Air Outlet

Water Drains

:

Best Available Copy

Generally, for normal temperature applications, recirculation from the Type W ROTO Generally, for normal temperature applications, recirculation from the type W MOTO-CLONE is practical without reheat. Temperature change or moisture increase is moderate. The exit dry buib temperature from the Type W will elways be less than the inlet temperature provided the latter exceeds the temperature of the spray water. For normal inlet velocities, the humidifying efficiency is approximately 50%, there-fore, moisture increase in the air stream is not enough to cause condensation in the average plant or work area. Actual temperature change and moisture increase can be easily determined.

Low Temperature: The humidifying action of the Type W ROTO-CLONE can be treated in terms of adiabatic addition of moisture to the air and the heat gain through the unit. The addition of heat may be assumed to take place at constant moisture content (dew point temperature) and the moisture addition at constant total heat content. In making these assumptions, the heat transfer between the air and water due to any temperature differential, which may exist, is neglected as is any condensation or re-evaporation of moisture through the unit. The moisture gain can be determined by the equation defining humidifying efficiency:

Νh $= (X_2 - X_1) \dots$

X₁ = moisture content of inlet air, grains

The sensible heat gain of an air mover has two components, fan inefficiency and heat of compression. However, where fan inefficiency is determined by test, both of these energy components are included in the differential between horsepower input (BHP) to the fan and air horsepower (AHP). Ignoring heat loss through the housing, tests have shown that the sensible heat gain through the Type W ROTO-CLONE to be approximately 0.25 BTU per pound of dry air per inch water gage of fan Total Pressure. The temperature rise of the air stream due to this heat gain approximates 1°F per linch water gage of fan Total Pressure. inch water gage of fan Total Pressure.

A portion of this sensible heat gain is converted to the latent heat of the moisture absorbed by the air. Since the evaporation of 1 grain of moisture will adiabatically reduce the temperature by $0.62^{\circ}F$, the temperature reduction of the air due to loss of sensible heat is $0.62~(X_2 - X_1)$. Taking both sensible and latent heat changes into consideration, this temperature change of the air leaving the Type W results in:

Data required to determine the humidifying efficiency of the Type W are CFM. Total Pressure, Size, Arrangement, inlet Dry Bulb Temperature, and Relative Humidity or Inlet Wet Bulb Temperature.

EXAMPLE: A No. 8 Type W, Arrangement A, ROTO-CLONE is exhausting 1400 cfm at 6" TP. Inlet air is at 70°F and 50% relative humidity. Find the moisture increase and the temperature of the air leaving the ROTO-CLONE, Point "A" on the psychroand the temperature of the air leaving the ROTO-CLONE, Point "A" on the psychrometric chart (Fig. 13) represents the entering air conditions of 70°F and 50% relative humidity. The addition of heat from Equation 2 is (.25 × 6" (")" = 1.5 BTU per pound of dry air. Point "B" indicates the heat content of the entering air and by adding the 1.5 BTU gain, point "C" is located on the total heat scale. Following the line of constant total heat corresponding with point "C", locates point "C" at the intersection of this total heat line and the 100% relative humidity or saturation line. Point "D" would represent the condition of the exit air if the ROTO-CLONE had a 100% humidifying efficiency, 1400 cfm in a No. 8 Type W ROTO-CLONE had a 4,000 fpm Inlet velocity. Fig. 13 shows the humidifying efficiency to be 53% for Arrangement A and 4,000 fpm velocity. Therefore, the exit condition along the same total heat line can be located by using Equation 1 and substituting N h = 53%, X'₂ = 80 grains (point "F"), X₁ = 55 grains (point "F"). Therefore, $X_2 = Nh (X'_2 - X_1) + X_1 = 0.53 (80 - 55) + 55 = 68.3$ grains per pound of dry air

Following the same total heat line until it intersects the horizontal line for 68.3 grains per pound of dry air, locates the exit condition, point "G". Note the exit dry bulb temperature is 67.8° F, relative hundity is 68% and moisture increase is $(X_2 - X_1)$ = 13.3 grains per pound of dry air.

A check on the result or a quick method of determining the temperature change can be obtained by using Equation 4.

 $\Delta t = (TP) - 0.62 (X_2 - X_1)$ = (6) - 0.62 (68.3 - 55) = -2.25°F

Therefore, 70°F — 2.25°F = 67.75°F which agrees with exit temperature of 67.8° found on the psychrometric chart.

High Temperature: Recirculation would never be used on processes involving high righ remperature exhaust gases. Additional spray nozzles are necessary for temperatures over 200°F to avoid evaporation of the normal water requirements. Assuming the spray nozzles in the inlet duct will have a humidifying efficiency of 50%, the equation to determine the quantity of water required to cool the inlet gases to 200°F is: W = M(ti - 200)

16,800

W = water, gpm; M = air, pounds per minute; tl = inlet temperature, degrees F

For more information, write American Air Filter Company, Inc.

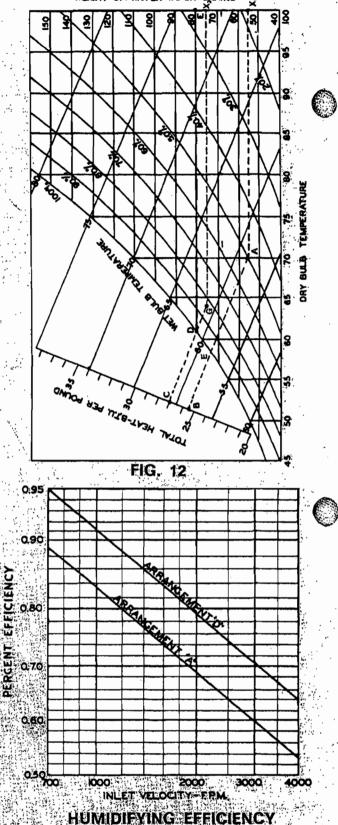


FIG. 13

American Air Filter has a policy of continuous product research and improvement and reserves the right to change design and specifications without notice.



Better Air is Our Business®

	AAE
í	INTERNATIONAL
Ì	215 CENTRAL AVENUE LOUISVILLE KY 40208-1406
	P O BOX 35690 LOUISVILLE KY 40232-5890



From:

Rick Stewart
Answer Center Technical Support
(800) 705-9290 (For Answer Center)

Phone No.:

(502) 537-0299

Paul Wesson

Relum FAX No.:

Date:

Page 1 of: Subject:

Company:

FAX No.:

RotoClone Efficiency

¢c:

January 12, 1996

Paul:

We do not have any efficiency ratings on skimmer. Here are some efficiency ratings on the W Rotoclone and much smaller micron than we discussed yesterday. Also, I'm sending a copy of the capacity table for the # 27.

Particle Size	<u>Efficiency</u>
2 μm	88.2 %
10 µm	99.0 %
•	99.65 %
16 µm	99.8 %
20 μm	99.9 %
26 µM	99.8 70

Hope this Information is helpful.

Rick Stewart

Section [3] of [9] Sugar Refinery

III. EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Application - For Title V air operation permitting only, emissions units are classified as regulated, unregulated, or insignificant. If this is an application for Title V air operation permit, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each regulated and unregulated emissions unit addressed in this application for air permit. Some of the subsections comprising the Emissions Unit Information Section of the form are optional for unregulated emissions units. Each such subsection is appropriately marked. Insignificant emissions units are required to be listed at Section II, Subsection C.

Air Construction Permit or FESOP Application - For air construction permitting or federally enforceable state air operation permitting, emissions units are classified as either subject to air permitting or exempt from air permitting. The concept of an "unregulated emissions unit" does not apply. If this is an application for air construction permit or FESOP, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air permitting are required to be listed at Section II, Subsection C.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit Application — Where this application is used to apply for both an air construction permit and a revised/renewal Title V air operation permit, each emissions unit is classified as either subject to air permitting or exempt from air permitting for air construction permitting purposes and as regulated, unregulated, or insignificant for Title V air operation permitting purposes. The air construction permitting classification must be used to complete the Emissions Unit Information Section of this application for air permit. A separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air construction permitting and insignificant emissions units are required to be listed at Section II, Subsection C.

If submitting the application form in hard copy, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application must be indicated in the space provided at the top of each page.

Section [3] Sugar Refinery

of [9]

A. GENERAL EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Emissions Unit Classification

1.	Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)									
	☐ The emis emissions			in this Emissio	ns U	Init Information S	ecti	on is a regulated		
			s unit addressed missions unit.	in this Emissio	ns U	Init Information S	ecti	on is an		
<u>En</u>	Emissions Unit Description and Status									
1.	Type of Emis	ssio	ns Unit Addresse	d in this Section	n: (Check one)				
						es, as a single em				
	•	_	oduction unit, or least one definab	<u> </u>	•	duces one or more	e an	pollutants and		
				•	`	,	issi	ons unit, a group of		
	☐ This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.									
						es, as a single em hich produce fugi				
2.	Description of Sugar Refine		nissions Unit Ad	ldressed in this	Sec	tion:				
3.	Emissions U	nit I	dentification Nur	nber: 021-025,	034	035				
4.	Emissions	5.	Commence	6. Initial	7.	Emissions Unit	8.	Acid Rain Unit?		
•	Unit Status Code:		Construction Date:	Startup Date:		Major Group SIC Code:		□ Yes ⊠ No		
	A		Date.	Date.		20		№ 140		
9.	Package Unit			<u>. </u>				-		
1.0	Manufacture		1		Mo	del Number:				
	Generator N		<u> </u>	MW						
11.	sent from the rail car. The	iner sug majo	y produces stand par mill. Some of	the refined sug d sugar produc	jar is	a specialty sugar s sold in bulk and s transferred by tro	ship	pped by truck on		
				·						

Section [3] of [9] Sugar Refinery

Emissions Unit Control Equipment

1.	Control Equipment	/Method(s) Descri	iption:			
	Baghouse			•		
	Wet Cyclonic Separ	ators (4)				
	Process Enclosed					
					<i>,</i>	
			·			
		•			·	
	ı					
2.	Control Device or I	Method Code(s):	018, 057, 054			

Section [3] Sugar Refinery of [9]

B. EMISSIONS UNIT CAPACITY INFORMATION

(Optional for unregulated emissions units.)

Emissions Unit Operating Capacity and Schedule

1.	Maximum Process or Throughp	out Rate:					
2.	Maximum Production Rate: 39	0,000 TPY					
3.	Maximum Heat Input Rate:	million Btu/hr					
4.	Maximum Incineration Rate:	pounds/hr					
		tons/day					
5. Requested Maximum Operating Schedule:							
		24 hours/day	7 days/week				
		52 weeks/year	8,760 hours/year				
	Operating Capacity/Schedule C	Comment:					
6.	Maximum production rate refers	s to the amount of refined su					
o.	Maximum production rate refers	s to the amount of refined su					

Section [3] Sugar Refinery of [9]

C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

Emission Point Description and Type

1.	Identification of Point on Plot Plan or Flow Diagram: See comment.			Emission Point 7	Type Code:		
3.	Descriptions of Emission		thi	s Emissions Unit	for VE Tracking:		
	See Attachment OC-EU3-C	15.					
	<u> </u>						
4.	ID Numbers or Descriptio	ns of Emission Un	its v	with this Emission	n Point in Common:		
5.	Discharge Type Code: V	6. Stack Height93 feet	•		7. Exit Diameter:2.5 feet		
8.	Exit Temperature: 100 °F	9. Actual Volum 15,000 acfm	netr	ic Flow Rate:	10. Water Vapor: %		
11.	Maximum Dry Standard F dscfm	low Rate:	12. Nonstack Emission Point Height: feet				
13.	Emission Point UTM Coo Zone: East (km):	rdinates	14. Emission Point Latitude/Longitude Latitude (DD/MM/SS)				
	North (km)		Longitude (DD/MM/SS)				
15.	Emission Point Comment:						
•	See Attachment OC-EU3-C stack parameters included				toclone No. 1. All other		
		,		,			
					•		
	,						

Section [3] Sugar Refinery

of [9]

D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment Description and Rate: Segment 1 of 3

1.	1. Segment Description (Process/Fuel Type):								
	Food and Agriculture - Sugar Cane Processing, General								
2.	Source Classification Cod 3-02-015-01	e (SCC):	3. SCC Units: Tons Sugar						
4.	Maximum Hourly Rate: 100	5. Maximum 390,000	Annual Rate:	6. Estimated Annual Activity Factor:					
7.	Maximum % Sulfur:	8. Maximum	% Ash:	9. Million Btu per SCC Unit:					
	10. Segment Comment: Maximum hourly and annual rates refer to the amount of refined sugar produced by the refinery from the fluidized bed and rotary drying systems. Maximum process rates for either system are 50 TPH and 1,200 TPD. Maximum process rates while operating both drying systems simultaneously are 100 TPH and 1,500 TPD.								
<u>Se</u>	gment Description and Ra	nte: Segment 2 o	of <u>3</u>						
1.	Segment Description (Pro	cess/Fuel Type):							
	Food and Agriculture - Sugar Cane Processing, Other Not Classified								
2.	Source Classification Cod 3-02-015-99	e (SCC):	3. SCC Units: Tons Proce						
4.	Maximum Hourly Rate:	5. Maximum 117,000	Annual Rate:	6. Estimated Annual Activity Factor:					

8. Maximum % Ash:

Maximum hourly and maximum annual rates refer to the maximum amount of refined sugar that could be loaded at the bulk load-out area. Annual operating hours are

DEP Form No. 62-210.900(1) – Form Effective: 06/16/03

7. Maximum % Sulfur:

10. Segment Comment:

8,760 hours.

9. Million Btu per SCC Unit:

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of [9]

Sugar Refinery

D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment Description and Rate: Segment 3 of 3

1.	Segment Description (Process/Fuel Type):							
	Food and Agriculture - Sugar Cane Processing, Other Not Classified							
			_					
2.	Source Classification Cod 3-02-015-99	e (SCC):	3. SCC Units: Tons Proce					
4.	Maximum Hourly Rate: 72	5. Maximum 273,000	Annual Rate:	6. Estimated Annual Activity Factor:				
7.	Maximum % Sulfur:	8. Maximum	% Ash:	9. Million Btu per SCC Unit:				
10.	Segment Comment:							
	Maximum hourly and annu could be loaded at the tran							
	8,760 hours.	•		, 0				
	·		·					
Se	gment Description and Ra	ite: Segment	of					
1.	Segment Description (Pro-	cess/Fuel Type):		į.				
	•							
2.	Source Classification Cod	e (SCC):	3. SCC Units:	:				
4.	Maximum Hourly Rate:	5. Maximum	Annual Rate:	6. Estimated Annual Activity Factor:				
7.	Maximum % Sulfur:	8. Maximum	% Ash:	9. Million Btu per SCC Unit:				
10.	Segment Comment:			•				
	•		•	•				
		•						
	·	_	,	·				

Section [3] Sugar Refinery

of [9]

E. EMISSIONS UNIT POLLUTANTS

List of Pollutants Emitted by Emissions Unit

1.	Pollutant Emitted	Primary Control Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
	PM	057, 018	054	EL
-	PM ₁₀	057, 018	054	EL '
	VOC			NS
		,		
ļ				
			,	
		-		
		-		
			1.	
				,
	· ·			
		,		
		-		

Section [3] of [9] Sugar Refinery

POLLUTANT DETAIL INFORMATION

Page [1] of [2] Particulate Matter Total - PM

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted: PM	2. Total Percent Efficiency of Control: 99.4		
3.	Potential Emissions:		4. Synth	netically Limited?
	7.06 lb/hour 17.06	tons/year	⊠ Ye	es 🗌 No
5.	Range of Estimated Fugitive Emissions (as to tons/year	applicable):		
6.	Emission Factor:			7. Emissions Method Code:
	Reference: Attachment OC-EU3-F1.8			2
8.	Calculation of Emissions:	•		
0	Total potential hourly and annual emissions (fluidized bed and rotary systems combined) Attachment OC-EU3-F1.8.	and load-out o	perations.	
9.	Pollutant Potential/Estimated Fugitive Emis See Attachment OC-EU3-F1.8 for complete c equipment.	and the second s		on of control

Section [3] of [9] Sugar Refinery

POLLUTANT DETAIL INFORMATION

Page [1] of [2] Particulate Matter Total - PM

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions Allowable Emissions 1 of 1

1.	Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions:
-	36.80 TPY	21.66 lb/hour 36.80 tons/year
	Method of Compliance: EPA Method 9	
6.	Allowable Emissions Comment (Description Based on permit No. 0990005-005-AC.	n of Operating Method):
Al	lowable Emissions Allowable Emissions	of
1.	Basis for Allowable Emissions Code:	2. Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4. Equivalent Allowable Emissions:
		lb/hour tons/year
5.	Method of Compliance:	
6.	Allowable Emissions Comment (Description	n of Operating Method):
,		
Al	lowable Emissions Allowable Emissions	of
	Tillowable Emissions	
1.	Basis for Allowable Emissions Code:	Emissions: Tuture Effective Date of Allowable Emissions:
		Future Effective Date of Allowable Emissions: Equivalent Allowable Emissions:
3.	Basis for Allowable Emissions Code: Allowable Emissions and Units:	2. Future Effective Date of Allowable Emissions:
3.	Basis for Allowable Emissions Code:	Future Effective Date of Allowable Emissions: Equivalent Allowable Emissions:
3. 5.	Basis for Allowable Emissions Code: Allowable Emissions and Units:	Future Effective Date of Allowable Emissions: Equivalent Allowable Emissions: lb/hour tons/year

Section [3] of [9] Sugar Refinery

POLLUTANT DETAIL INFORMATION

Page [2] of [2] Particulate Matter - PM₁₀

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted: PM ₁₀	2. Total Perc 99.0%	ent Efficie	ency of Control:
3.	Potential Emissions:			netically Limited?
	1.54 lb/hour 2.40	tons/year	⊠ Ye	es No
5.	Range of Estimated Fugitive Emissions (as to tons/year	applicable):		
6.	Emission Factor:			7. Emissions Method Code:
	Reference: Attachment OC-EU3-F1.8.			2
8.	Calculation of Emissions:			
9.	Total potential hourly emissions from sugar load-out operations. Total potential annual enhandling (fluidized bed and rotary systems of Attachment OC-EU3-F1.8. Pollutant Potential/Estimated Fugitive Emis	emissions repre combined) and l	sent suga oad-out op	r drying and
9.	Pollutant Potential/Estimated Fugitive Emis See Attachment OC-EU3-F1.8 for complete c equipment.			on of control

Section [3] of [9] Sugar Refinery

POLLUTANT DETAIL INFORMATION

Page [2] of [2] Particulate Matter - PM₁₀

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions 1 of 1

1.	Basis for Allowable Emissions Code: OTHER	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units: 13.39 TPY	4.	Equivalent Allowable Emissions: 10.0 lb/hour 13.39 tons/year
5.	Method of Compliance: EPA Method 9		
6.	Allowable Emissions Comment (Description Based on permit No. 0990005-005-AC.	of C	Operating Method):
<u>Al</u>	lowable Emissions Allowable Emissions	o	f
1.	Basis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance:		
6.	Allowable Emissions Comment (Description	of C	perating Method):
Al	lowable Emissions Allowable Emissions	o:	f
.1.	Basis for Allowable Emissions Code:		Future Effective Date of Allowable Emissions:
3.	Allowable Emissions and Units:	4.	Equivalent Allowable Emissions: 1b/hour tons/year
5.	Method of Compliance:		
6.	Allowable Emissions Comment (Description	of C	Operating Method):

Section [3]

of [9]

Sugar Refinery

G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

Visible Emissions Limitation: Visible Emissions Limitation 1 of 2

1.	Visible Emissions Subtype:	2. Basis for Allowable Or	pacity:
	VE.	⊠ Rule [Other
3.	Allowable Opacity:		
		ceptional Conditions:	%
	Maximum Period of Excess Opacity Allowe	ed:	min/hour
4.	Method of Compliance: EPA Method 9	-	
5.	Visible Emissions Comment: Rule 62-297.620(4), F.A.C. and Permit No. 09 source exhaust stack, and is requested in lie		olies to each point
Vi	sible Emissions Limitation: Visible Emissi	ons Limitation <u>2</u> of <u>2</u>	
1.	Visible Emissions Subtype:	2. Basis for Allowable Op	pacity:
	VE	⊠ Rule [Other
3.	Allowable Opacity: Normal Conditions: 20 % Ex Maximum Period of Excess Opacity Allower	ceptional Conditions:	% min/hour
4.	Method of Compliance: EPA Method 9		
5.	Visible Emissions Comment:	·	
5.	Rule 62-296.310(2), F.A.C. This limit applies	to all fugitive emission point	ts.
	•		

Section [3] Sugar Refinery

of [9]

H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

<u>C0</u>	numuous Monitoring System: Continuous	IVIOI	Intol 01	
1.	Parameter Code:	2.	Pollutant(s):	
3.	CMS Requirement:		Rule	Other
4.	Monitor Information Manufacturer:			
	Model Number:		Serial Number	er:
5.	Installation Date:	6.	Performance Spe	ecification Test Date:
7.	Continuous Monitor Comment:			
Co	ontinuous Monitoring System: Continuous	Moi	nitor of	
1.	Parameter Code:		2. Pollutant(s):	
3.	CMS Requirement:		Rule	Other
4.	Monitor Information Manufacturer: Model Number:		Serial Numbe	·
				<u> </u>
5.	Installation Date:		6. Performance	Specification Test Date:
7.	Continuous Monitor Comment:		•	

Section [3] Sugar Refinery of [9]

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: OC-EU3-I1 Previously Submitted, Date
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: OC-EU3-I3 Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Previously Submitted, Date
5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Previously Submitted, Date Not Applicable
6.	Compliance Demonstration Reports/Records Attached, Document ID: Test Date(s)/Pollutant(s) Tested:
	☐ Previously Submitted, Date: Test Date(s)/Pollutant(s) Tested:
	∑ To be Submitted, Date (if known): Test Date(s)/Pollutant(s) Tested: VE
	☐ Not Applicable
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute ☐ Attached, Document ID:

Section [3] of [9] Sugar Refinery

Additional Requirements for Air Construction Permit Applications

1. Control Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7),
F.A.C.; 40 CFR 63.43(d) and (e))
☐ Attached, Document ID: ☐ Not Applicable
2. Good Engineering Practice Stack Height Analysis (Rule 62-212.400(5)(h)6., F.A.C., and
Rule 62-212.500(4)(f), F.A.C.)
☐ Attached, Document ID: ☐ Not Applicable
3. Description of Stack Sampling Facilities (Required for proposed new stack sampling
facilities only)
☐ Attached, Document ID: ☐ Not Applicable
Additional Requirements for Title V Air Operation Permit Applications
1. Identification of Applicable Requirements
☐ Attached, Document ID: OC-EU3-IV1 ☐ Not Applicable
2. Compliance Assurance Monitoring
☐ Attached, Document ID: <u>CAM Plan</u> ☐ Not Applicable
3. Alternative Methods of Operation
☐ Attached, Document ID: OC-EU3-I1 ☐ Not Applicable
4. Alternative Modes of Operation (Emissions Trading)
☐ Attached, Document ID: ☐ Not Applicable
5. Acid Rain Part Application
☐ Certificate of Representation (EPA Form No. 7610-1)
☐ Copy Attached, Document ID:
☐ Acid Rain Part (Form No. 62-210.900(1)(a))
Attached, Document ID:
☐ Previously Submitted, Date:
☐ Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
Attached, Document ID:
☐ Previously Submitted, Date:
☐ New Unit Exemption (Form No. 62-210.900(1)(a)2.)
Attached, Document ID:
☐ Previously Submitted, Date:
☐ Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)
Attached, Document ID:
☐ Previously Submitted, Date:
☐ Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)
Attached, Document ID:
☐ Previously Submitted, Date:
☐ Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)
Attached, Document ID:
☐ Previously Submitted, Date:
Not Applicable ■

Additional Requirements Comment

EMISSIONS UNIT INFORMATION

of

[9]

Section [3]

EMISSIONS UNIT INFORMATION Section [4] of [9] Paint Spray Booth

III. EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Application - For Title V air operation permitting only, emissions units are classified as regulated, unregulated, or insignificant. If this is an application for Title V air operation permit, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each regulated and unregulated emissions unit addressed in this application for air permit. Some of the subsections comprising the Emissions Unit Information Section of the form are optional for unregulated emissions units. Each such subsection is appropriately marked. Insignificant emissions units are required to be listed at Section II, Subsection C.

Air Construction Permit or FESOP Application - For air construction permitting or federally enforceable state air operation permitting, emissions units are classified as either subject to air permitting or exempt from air permitting. The concept of an "unregulated emissions unit" does not apply. If this is an application for air construction permit or FESOP, a separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air permitting are required to be listed at Section II, Subsection C.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit Application — Where this application is used to apply for both an air construction permit and a revised/renewal Title V air operation permit, each emissions unit is classified as either subject to air permitting or exempt from air permitting for air construction permitting purposes and as regulated, unregulated, or insignificant for Title V air operation permitting purposes. The air construction permitting classification must be used to complete the Emissions Unit Information Section of this application for air permit. A separate Emissions Unit Information Section (including subsections A through I as required) must be completed for each emissions unit subject to air permitting addressed in this application for air permit. Emissions units exempt from air construction permitting and insignificant emissions units are required to be listed at Section II, Subsection C.

If submitting the application form in hard copy, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application must be indicated in the space provided at the top of each page.

EMISSIONS UNIT INFORMATION Section [4] of [9]

Paint Spray Booth

A. GENERAL EMISSIONS UNIT INFORMATION

Title V Air Operation Permit Emissions Unit Classification

1.	Regulated or Unregulated Emissions Unit? (Check one, if applying for an initial, revised or renewal Title V air operation permit. Skip this item if applying for an air construction permit or FESOP only.)						
	 ☑ The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit. ☐ The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit. 						
<u>E</u> n	nissions Unit	Description and Sta	<u>itus</u>				
1.	Type of Emi	ssions Unit Addresse	d in this Section	on: (Check one)			
	process o		activity, which	dresses, as a single em a produces one or more int (stack or vent).			
	process		nd activities wh	ich has at least one de	issions unit, a group of finable emission point		
			· ·	dresses, as a single em es which produce fug	· · · · · · · · · · · · · · · · · · ·		
2.	2. Description of Emissions Unit Addressed in this Section: Paint Spray Booth						
3.	Emissions U	nit Identification Nui	mber: 048				
4.	Emissions Unit Status Code:	5. Commence Construction Date:	6. Initial Startup Date:	7. Emissions Unit Major Group SIC Code: 07	8. Acid Rain Unit? ☐ Yes ☑ No		
9.	Package Uni Manufacture	t: Paint Spray Booth r: AFC, Inc.		Model Number: TSD	6036		
10	. Generator N	lameplate Rating:	MW				
11	11. Emissions Unit Comment: A Crossflo truck spray booth.						

Section [4] of [9] Paint Spray Booth

Emissions Unit Control Equipment

1.	Control Equipment/Method(s) Description:				
	Glass fiber paint arrestor pad				
•					
2	Control Daviss or Mathad Code(a): 050				

Section [4]
Paint Spray Booth

of [9]

B. EMISSIONS UNIT CAPACITY INFORMATION

(Optional for unregulated emissions units.)

Emissions Unit Operating Capacity and Schedule

C 1	1. Maximum Process or Throughput Rate: 4,950 gallons/year				
Maximum Production Rate:					
Maximum Heat Input Rate:	million Btu/hr				
Maximum Incineration Rate:	pounds/hr				
	tons/day				
5. Requested Maximum Operating Schedule:					
	24 hours/day	7 days/week			
	52 weeks/year	8,760 hours/year			
Operating Capacity/Schedule Co	omment:	·			
	Maximum Heat Input Rate: Maximum Incineration Rate: Requested Maximum Operating Operating Capacity/Schedule Co	Maximum Heat Input Rate: million Btu/hr Maximum Incineration Rate: pounds/hr tons/day Requested Maximum Operating Schedule: 24 hours/day			

Section [4] o

of [9]

C. EMISSION POINT (STACK/VENT) INFORMATION (Optional for unregulated emissions units.)

Emission Point Description and Type

1.	Identification of Point on Plot Plan or Flow Diagram: Paint Spray Booth		2. Emission Point Type Code: 3		
3.	Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking:				
,	Two identical exhaust stacks.				
4.	ID Numbers or Descriptio	ns of Emission U	nits with this Emission	n Point in Common:	
5.	Discharge Type Code: v	6. Stack Height: 25.7 feet		7. Exit Diameter: 4 feet	
8.	Exit Temperature: 77 °F	9. Actual Volumetric Flow Rate: 45,500 acfm		10. Water Vapor: %	
11	. Maximum Dry Standard F dscfm	low Rate:	12. Nonstack Emission Point Height: feet		
13	Emission Point UTM Coo Zone: East (km):	rdinates	14. Emission Point Latitude/Longitude Latitude (DD/MM/SS)		
	North (km)	:	Longitude (DD/MM/SS)		
15. Emission Point Comment: There are two exhaust stacks for the Paint Spray Booth. Both are 25.7 ft tall with a 4-ft diameter and have a flow rate of 45,500 acfm.					
			,		

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Paint Spray Booth

D. SEGMENT (PROCESS/FUEL) INFORMATION

Segment Description and Rate: Segment 1 of 1

1.	1. Segment Description (Process/Fuel Type):					
	Surface Coating Application General - Paint: Solvent Based					
2	Carros Classification Cod	. (0)	CC).	3. SCC Units:		
2.	Source Classification Code 4-02-001-10	3 (3)	CC):	Gallons of c	oati	ngs
4.	Maximum Hourly Rate: 16.8	5.	Maximum 4,950	Annual Rate:	6.	Estimated Annual Activity Factor:
7.	Maximum % Sulfur:	8.	Maximum	% Ash:	9.	Million Btu per SCC Unit:
10	Segment Comment:					
Se	gment Description and Ra	te:	Segment	of		
1.	Segment Description (Prod	cess/	Fuel Type):	•		
	•			•		
2.	Source Classification Code	e (So	CC):	3. SCC Units:		
4.	Maximum Hourly Rate:	5.	Maximum	Annual Rate:	6.	Estimated Annual Activity Factor:
7.	Maximum % Sulfur:	8.	Maximum	% Ash:	9.	Million Btu per SCC Unit:
10. Segment Comment:						
		٠				

Section [4] of [9] Paint Spray Booth

E. EMISSIONS UNIT POLLUTANTS

List of Pollutants Emitted by Emissions Unit

1.	Pollutant Emitted	Primary Control Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
	VOC			EL
	·			
		_		
\vdash				
	•			
	<u> </u>	•	· ·	
	·			

EMISSIONS UNIT INFORMATION

Section [4] of [9] Paint Spray Booth

POLLUTANT DETAIL INFORMATION

Page [1] of [1] Volatile Organic Compounds - VOC

F1. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION – POTENTIAL/ESTIMATED FUGITIVE EMISSIONS

(Optional for unregulated emissions units.)

Potential/Estimated Fugitive Emissions

Complete for each pollutant identified in Subsection E if applying for an air construction permit or concurrent processing of an air construction permit and a revised or renewal Title V permit. Complete for each emissions-limited pollutant identified in Subsection E if applying for an air operation permit.

1.	Pollutant Emitted: VOC	2. Total Perc	ent Efficie	ency of Control:
3.	Potential Emissions:		4. Synth	netically Limited?
	70.4 lb/hour 9.40	tons/year	⊠Y€	es 🗌 No
5.	Range of Estimated Fugitive Emissions (as	applicable):		
	to tons/year			<u> </u>
6.	Emission Factor:			7. Emissions
	D (_		Method Code:
	Reference: Permit No. 0990005-015-A	.C		0
8.	Calculation of Emissions:			
	See Attachment OC-EU4-F1.8 for calculation	s.		
				•
	,			
				•
9.	Pollutant Potential/Estimated Fugitive Emis	sions Commen	t:	•

DEP Form No. 62-210.900(1) – Form Effective: 06/16/03

EMISSIONS UNIT INFORMATION Section [4] of [9]

Paint Spray Booth

POLLUTANT DETAIL INFORMATION
Page [1] of [1]
Volatile Organic Compounds - VOC

F2. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION - ALLOWABLE EMISSIONS

Complete if the pollutant identified in Subsection F1 is or would be subject to a numerical emissions limitation.

Allowable Emissions of				
1. Bas	sis for Allowable Emissions Code: ner	2.	Future Effective Date of Allowable Emissions:	
	owable Emissions and Units: 0 tons per year	4.	Equivalent Allowable Emissions: lb/hour 9.40 tons/year	
	ethod of Compliance: nthly usage and VOC tracking.			
	:			
6. Allowable Emissions Comment (Description of Operating Method): Based on Permit No. 0990005-015-AC, limit is on a 12-consecutive-month basis.				
Allowa	able Emissions Allowable Emissions	c	of	
1. Bas	sis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:	
3. All	owable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/yea	ır
5. Me	ethod of Compliance:		•	
6. Allowable Emissions Comment (Description of Operating Method):				
Allowable Emissions of				
1. Bas	sis for Allowable Emissions Code:	2.	Future Effective Date of Allowable Emissions:	
3. All	owable Emissions and Units:	4.	Equivalent Allowable Emissions: lb/hour tons/yea	ar
5. Me	ethod of Compliance:			
6. All	owable Emissions Comment (Description	of (Operating Method):	

EMISSIONS UNIT INFORMATION

Section [4]
Paint Spray Booth

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G. VISIBLE EMISSIONS INFORMATION

Complete if this emissions unit is or would be subject to a unit-specific visible emissions limitation.

Visible Emissions Limitation: Visible Emissions Limitation 1 of 2

1.	Visible Emissions Subtype: VE20	2. Basis for Allowable ⊠ Rule	Opacity: ☐ Other
3.	Allowable Opacity: Normal Conditions: Maximum Period of Excess Opacity Allow	ceptional Conditions:	% min/hour
4.	Method of Compliance: EPA Method 9		
5.	Visible Emissions Comment: Rule 62-296.320, F.A.C.	·	
Vis	sible Emissions Limitation: Visible Emissi	ions Limitation of _	
1.	Visible Emissions Subtype:	2. Basis for Allowable ☐ Rule	Opacity: Other
		Kuie	
3.	Allowable Opacity: Normal Conditions: % Ex Maximum Period of Excess Opacity Allow	xceptional Conditions:	% min/hour
	Normal Conditions: % Ex	xceptional Conditions:	· -
4.	Normal Conditions: % Ex Maximum Period of Excess Opacity Allow	xceptional Conditions:	

EMISSIONS UNIT INFORMATION

Section [4] Paint Spray Booth

of [9]

H. CONTINUOUS MONITOR INFORMATION

Complete if this emissions unit is or would be subject to continuous monitoring.

<u>Co</u>	Continuous Monitoring System: Continuous Monitor of		
1.	Parameter Code:	2.	Pollutant(s):
3.	CMS Requirement:		Rule
4.	Monitor Information Manufacturer:		
	Model Number:		Serial Number:
5.	Installation Date:	6.	Performance Specification Test Date:
7.	Continuous Monitor Comment:		
Co	ntinuous Monitoring System: Continuous	Moi	nitor of
1.	Parameter Code:		2. Pollutant(s):
3.	CMS Requirement:		Rule
4.	Monitor Information Manufacturer:		•
	Model Number:		Serial Number:
5.	<u> </u>		6. Performance Specification Test Date:
٦.	installation Date.		o. Teriormance Specification Test Date.
7.	Continuous Monitor Comment:		

EMISSIONS UNIT INFORMATION Section [4] of [9] Paint Spray Booth

I. EMISSIONS UNIT ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1.	Process Flow Diagram (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: OC-EU4-I1 Previously Submitted, Date
2.	Fuel Analysis or Specification (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Previously Submitted, Date
3.	Detailed Description of Control Equipment (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: OC-EU4-13 Previously Submitted, Date
4.	Procedures for Startup and Shutdown (Required for all operation permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Previously Submitted, Date
	Not Applicable (construction application)
5.	Operation and Maintenance Plan (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought) Attached, Document ID: Previously Submitted, Date
	Not Applicable ■
6.	Compliance Demonstration Reports/Records Attached, Document ID: Test Date(s)/Pollutant(s) Tested:
	Previously Submitted, Date: Test Date(s)/Pollutant(s) Tested:
	☐ To be Submitted, Date (if known): Test Date(s)/Pollutant(s) Tested:
	Not Applicable ■
	Note: For FESOP applications, all required compliance demonstration records/reports must be submitted at the time of application. For Title V air operation permit applications, all required compliance demonstration reports/records must be submitted at the time of application, or a compliance plan must be submitted at the time of application.
7.	Other Information Required by Rule or Statute Attached, Document ID: Not Applicable

DEP Form No. 62-210.900(1) – Form Effective: 06/16/03

EMISSIONS UNIT INFORMATION

Section [4] of [9] Paint Spray Booth

Additional Requirements for Air Construction Permit Applications

1.	Control Technology Review and Analysis (Rules 62-212.400(6) and 62-212.500(7),
	F.A.C.; 40 CFR 63.43(d) and (e))
	Attached, Document ID: Not Applicable
2.	Good Engineering Practice Stack Height Analysis (Rule 62-212.400(5)(h)6., F.A.C., and Rule 62-212.500(4)(f), F.A.C.)
	☐ Attached, Document ID: ☐ Not Applicable
3.	
].	facilities only)
	☐ Attached, Document ID: ☐ Not Applicable
<u>A</u>	dditional Requirements for Title V Air Operation Permit Applications
1.	Identification of Applicable Requirements
2.	Compliance Assurance Monitoring
3.	Alternative Methods of Operation
	☐ Attached, Document ID: ⊠ Not Applicable
4.	Alternative Modes of Operation (Emissions Trading)
	Attached, Document ID: Not Applicable
5.	Acid Rain Part Application
	Certificate of Representation (EPA Form No. 7610-1)
	Copy Attached, Document ID:
	☐ Acid Rain Part (Form No. 62-210.900(1)(a))
	Attached, Document ID:
	Previously Submitted, Date:
	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
	Attached, Document ID:
	Previously Submitted, Date:
	☐ New Unit Exemption (Form No. 62-210.900(1)(a)2.) ☐ Attached, Document ID:
	Previously Submitted, Date:
	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)
	Attached, Document ID:
	Previously Submitted, Date:
	☐ Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)
	Attached, Document ID:
	Previously Submitted, Date:
	☐ Phase II NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)
	Attached, Document ID:
	Previously Submitted, Date:

Additional Requirements Comment

EMISSIONS UNIT INFORMATION

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Section [4]

ATTACHMENT OC-EU4-IV1

IDENTIFICATION OF APPLICABLE REQUIREMENTS

Identification of Applicable Requirements

62-4.070(3)

62-4.160(2)

62-210.200

62.210.370

62-296.320(2)

62-296.320(4)(c)

62-297.310(7)(b)

PAINT SPRAY BOOTH PERMIT



GOLDER ASSOCIATES INC. Department of **Environmental Protection**

AUG - 3 2005

leb Bush Governor

South District P.O. Box 2549 Fort Myers, Florida 33902-2549

Colleen M. Castille Secretary

NOTICE OF INTENT TO ISSUE AIR CONSTRUCTION PERMIT MODIFICATION

August 1, 2005

CERTIFIED MAIL 7002 2410 0002 4843 2438 RETURN RECEIPT REQUESTED

In the Matter of an Application for Permit by:

Ricardo A. Lima Okeelanta Corporation 21250 U.S. Highway 27 South Bay, Florida 33493 Palm Beach County - AP Okeelanta Corporation Okeelanta Sugar Mill and Refinery DEP File No. 0990005-015-AC

Dear Mr. Lima:

Enclosed is one copy of the Draft air construction permit modification for Okeelanta Corporation located at 21250 U.S. Highway 27, South Bay, Palm Beach County. The Department's Intent to Issue Air Construction Permit Modification and the Public Notice of Intent to Issue Air Construction Permit Modification are also included.

The Public Notice of Intent to Issue Air Construction Permit Modification must be published one time only, as soon as possible, in the legal advertisement section of a newspaper of general circulation in the area affected, pursuant to the requirements Chapter 50, Florida Statutes. Proof of publication, i.e., newspaper affidavit, must be provided to the Department's South District Office within seven days of publication. Failure to publish the notice and provide proof of publication may result in the denial of the permit.

Please submit any written comments you wish to have considered concerning the Department's proposed action to Mr. Ronald D. Blackburn, District Air Program Administrator at the above letterhead address. If you have any other questions, please contact Mara G. Nasca, Environmental Manager at 332-6975, Ext. 188 or Deanna Newburg ext. 173.

Sincerely,

Jon M. Iglehart Director of

District Management

JMI/DLN/iw Enclosures

In the Matter of an Application for Permit by:

Ricardo A. Lima Okeelanta Corporation 21250 U.S. Highway 27 South Bay, Florida 33493 Palm Beach County - AP
Okeelanta Corporation
Okeelanta Sugar Mill and Refinery
DEP File No. 0990005-015-AC

INTENT TO ISSUE AIR CONSTRUCTION PERMIT MODIFICATION

The Department of Environmental Protection (Department) gives notice of its intent to issue an air construction permit modification (copy of Draft permit attached) for the proposed project, detailed in the application specified above for the reasons stated below.

The applicant, Okeelanta Corporation, applied on February 11, 2005, to the Department for an air construction permit modification for its Okeelanta Sugar Mill and Refinery located approximately six miles south of South Bay on U.S. Highway 27, South Bay, Palm Beach County. The permit modifies Construction Permit 0990005-010-AC to increase the permitted capacity of paint and thinner usage from 2,475 gallons per year to 4,950 gallons per year, modifies Construction Permit 0990005-013-AC to remove the RACT (reasonable available control technology) requirements, and then combines the permits. The paint booth has the potential to emit 0.35 tons per year of particulate matter (PM), 0.35 tons per year of PM10, 9.38 tons/year of volatile organic compound (VOC) and 0.47 tons per year of Hazardous Air Pollutants (HAPs). The Department has permitting jurisdiction under the provisions of Chapter 403, Florida Statutes (F.S.), and Florida Administrative Code (F.A.C.) Chapters 62-4, 62-210, and 62-212. The above actions are not exempt from permitting procedures. The Department has determined that an air construction permit is required for this project.

The Department intends to issue this air construction permit based on the belief that reasonable assurances have been provided to indicate that operation of these emission units will not adversely impact air quality, and the emission units will comply with all appropriate provisions of Chapters 62-4, 62-204, 62-210, 62-212, 62-296, and 62-297, F.A.C.

Pursuant to Section 403.815, F.S., and Rule 62-110.106(7)(a)1., F.A.C., you (the applicant) are required to publish at your own expense the enclosed Public Notice of Intent to Issue Air Construction Permit Modification. The notice shall be published one time only in the legal advertisement section of a newspaper of general circulation in the area affected. Rule 62-110.106(7)(b), F.A.C., requires that the applicant cause the notice to be published as soon as possible after notification by the Department of its intended action. For the purpose of these rules, "publication in a newspaper of general circulation in the area affected" means publication in a newspaper meeting the requirements of Sections 50.011 and 50.031, F.S., in the county where the activity is to take place. If you are uncertain that a newspaper meets these requirements, please contact the Department at the address or telephone number listed below. The applicant shall provide proof of publication to the Department of Environmental Protection, Post Office Box 2549, Fort Myers, Florida 33902-2549, (Telephone: (239) 332-6975, Fax: (239) 332-6969). You must provide proof of publication within seven days of publication, pursuant to Rule 62-110.106(5), F.A.C. No permitting action for which published notice is required shall be granted until proof of publication of notice is made by furnishing a uniform affidavit in substantially the form prescribed in Section 50.051, F.S. to the office of the Department issuing the permit. Failure to publish the notice and provide proof of publication may result in the denial of the permit pursuant to Rules 62-110.106(9) & (11), F.A.C.

The Department will issue the final permit with the attached conditions unless a response received in accordance with the following procedures results in a different decision or significant change of terms or conditions.

INTENT TO ISSUE AIR CONSTRUCTION PERMIT MODIFICATION Okeelanta Corporation DEP File No. 0990005-015-AC Page 2 of 4

The Department will accept written comments concerning the proposed permit issuance action for a period of fourteen days from the date of publication of <u>Public Notice of Intent to Issue Air Construction Permit Modification</u>. Written comments should be provided to the Department of Environmental Protection, Post Office Box 2549, Fort Myers, Florida 33902-2549. Any written comments filed shall be made available for public inspection. If written comments received result in a significant change in the proposed agency action, the Department shall revise the proposed permit and require, if applicable, another Public Notice.

The Department will issue the permit with the attached conditions unless a timely petition for an administrative hearing is filed pursuant to Sections 120.569 and 120.57 F.S., before the deadline for filing a petition. The procedures for petitioning for a hearing are set forth below.

A person whose substantial interests are affected by the proposed permitting decision may petition for an administrative proceeding (hearing) under Sections 120.569 and 120.57, F.S. The petition must contain the information set forth below and must be filed (received) in the Office of General Counsel of the Department of Environmental Protection, 3900 Commonwealth Boulevard, Mail Station #35, Tallahassee, Florida, 32399-3000. Petitions filed by the permit applicant or any of the parties listed below must be filed within fourteen days of receipt of this notice of intent. Petitions filed by any persons other than those entitled to written notice under Section 120.60(3), F.S. must be filed within fourteen days of publication of the public notice or within fourteen days of receipt of this notice of intent, whichever occurs first. Under Section 120.60(3), F.S., however, any person who asked the Department for notice of agency action may file a petition within fourteen days of receipt of that notice, regardless of the date of publication. A petitioner shall mail a copy of the petition to the applicant at the address indicated above at the time of filing. The failure of any person to file a petition within the appropriate time period shall constitute a waiver of that person's right to request an administrative determination (hearing) under Sections 120.569 and 120.57, F.S. or to intervene in this proceeding and participate as a party to it. Any subsequent intervention will be only at the approval of the presiding officer upon the filing of a motion in compliance with Rule 28-106.205, F.A.C.

A petition that disputes the material facts on which the Department's action is based must contain the following information: (a) The name and address of each agency affected and each agency's file or identification number, if known; (b) The name, address, and telephone number of the petitioner, the name, address, and telephone number of the petitioner's representative, if any, which shall be the address for service purposes during the course of the proceeding; and an explanation of how the petitioner's substantial interests will be affected by the agency determination; (c) A statement of how and when petitioner received notice of the agency action or proposed action; (d) A statement of all disputed issues of material fact. If there are none, the petition must so indicate; (e) A concise statement of the ultimate facts alleged, including the specific facts the petitioner contends warrant reversal or modification of the agency's proposed action; (f) A statement of the specific rules or statutes the petitioner contends require reversal or modification of the agency's proposed action; and (g) A statement of the relief sought by the petitioner, stating precisely the action petitioner wishes the agency to take with respect to the agency's proposed action.

A petition that does not dispute the material facts upon which the Department's action is based shall state that no such facts are in dispute and otherwise shall contain the same information as set forth above, as required by Rule 28-106.301, F.A.C.

Because the administrative hearing process is designed to formulate final agency action, the filing of a petition means that the Department's final action may be different from the position taken by it in this notice. Persons whose substantial interests will be affected by any such final decision of the Department

INTENT TO ISSUE AIR CONSTRUCTION PERMIT MODIFICATION Okeelanta Corporation
DEP File No. 0990005-015-AC
Page 3 of 4

on the application have the right to petition to become a party to the proceeding, in accordance with the requirements set forth above.

Mediation is not available in this proceeding.

In addition to the above, a person subject to regulation has a right to apply for a variance from or waiver of the requirements of particular rules, on certain conditions, under Section 120.542, F.S. The relief provided by this state statute applies only to state rules, not statutes, and not to any federal regulatory requirements. Applying for a variance or waiver does not substitute or extend the time for filing a petition for an administrative hearing or exercising any other right that a person may have in relation to the action proposed in this notice of intent.

The application for a variance or waiver is made by filing a petition with the Office of General Counsel of the Department of Environmental Protection, 3900 Commonwealth Boulevard, Mail Station #35, Tallahassee, Florida 32399-3000. The petition must specify the following information: (a) The name, address, and telephone number of the petitioner; (b) The name, address, and telephone number of the attorney or qualified representative of the petitioner, if any; (c) Each rule or portion of a rule from which a variance or waiver is requested; (d) The citation to the statute underlying (implemented by) the rule identified in (c) above; (e) The type of action requested; (f) The specific facts that would justify a variance or waiver for the petitioner; (g) The reason why the variance or waiver would serve the purposes of the underlying statute (implemented by the rule); and (h) A statement whether the variance or waiver is permanent or temporary and, if temporary, a statement of the dates showing the duration of the variance or waiver requested.

The Department will grant a variance or waiver when the petition demonstrates both that the application of the rule would create a substantial hardship or violate principles of fairness, as each of those terms is defined in Section 120.542(2), F.S. and that the purpose of the underlying statute will be or has been achieved by other means by the petitioner.

Persons subject to regulation pursuant to any federally delegated or approved air program should be aware that Florida is specifically not authorized to issue variances or waivers from any requirements of any such federally delegated or approved program. The requirements of the program remain fully enforceable by the Administrator of the EPA and by any person under the Clean Air Act unless and until the Administrator separately approves any variance or waiver in accordance with the procedures of the federal program.

Executed in Fort Myers, Florida.

STATE OF FLORIDA DEPARTMENT OF ENVIRONMENTAL PROTECTION

Jon M. Iglehart Director of

District Management

Post Office Box 2549

Fort Myers, Florida 33902-2549

(239) 332-6975

INTENT TO ISSUE AIR CONSTRUCTION PERMIT MODIFICATION Okeelanta Corporation DEP File No. 0990005-015-AC Page 4 of 4

CERTIFICATE OF SERVICE

The undersigned duly designated deputy agency clerk hereby certifies that this Intent to Issue Air
Construction Permit Modification (including the Public Notice of Intent to Issue Air Construction Permit
Modification and the Draft permit) was sent by certified mail (*) and copies were mailed by U.S. Mail
before the close of business on (leaust 1, 2005 to the persons listed:

Ricardo A. Lima, Vice-President -General Manager, Okeelanta Corporation * David A. Buff, P.E. – Golder Associates, Inc. V

James Stormer, Palm Beach County Air Program Administrator

Clerk Stamp

FILING AND ACKNOWLEDGMENT FILED, on this date, pursuant to \$120.52, Florida Statutes, with the designated Department Clerk, receipt of which is hereby acknowledged.

PUBLIC NOTICE OF INTENT TO ISSUE AIR CONSTRUCTION PERMIT MODIFICATION

STATE OF FLORIDA

DEPARTMENT OF ENVIRONMENTAL PROTECTION

DEP File No. 0990005-015-AC

Okeelanta Corporation

Okeelanta Sugar Mill and Refinery

Palm Beach County

The Department of Environmental Protection (Department) gives notice of its intent to issue an air construction permit modification to Okeelanta Corporation, for the Okeelanta Sugar Mill and Refinery located approximately six miles south of South Bay on US Highway 27, South Bay, Palm Beach County. The permit modifies Construction Permit 0990005-010-AC to increase the permitted capacity of paint and thinner usage from 2,475 gallons per year to 4,950 gallons per year, modifies Construction Permit 0990005-013-AC to remove the RACT (reasonable available control technology) requirements, and then combines the permits. The paint booth has the potential to emit 0.35 tons per year of particulate matter (PM), 0.35 tons per year of PM10, 9.38 tons/year of volatile organic compound (VOC) and 0.47 tons per year of Hazardous Air Pollutants (HAPs).

The Department will issue the Final permit with the attached conditions unless a response received in accordance with the following procedures results in a different decision or significant change of terms or conditions.

The Department will accept written comments concerning the proposed permit issuance action for a period of fourteen days from the date of publication of this Public Notice of Intent to Issue Air Construction Permit Modification. Written comments should be provided to the Department of Environmental Protection, Post Office Box 2549, Fort Myers, Florida 33902-2549. Any written comments filed shall be made available for public inspection. If written comments received result in a significant change in the proposed agency action, the Department shall revise the proposed permit and require, if applicable, another Public Notice.

The Department will issue the permit with the attached conditions unless a timely petition for an administrative hearing is filed pursuant to Sections 120.569 and 120.57, F.S. before the deadline for filing a petition. The procedures for petitioning for a hearing are set forth below.

Mediation is not available in this proceeding.

A person whose substantial interests are affected by the proposed permitting decision may petition for an administrative proceeding (hearing) under Sections 120.569 and 120.57, F.S. The petition must contain the information set forth below and must be filed (received) in the Office of General Counsel of the Department, 3900 Commonwealth Boulevard, Mail Station #35, Tallahassee, Florida, 32399-3000. Petitions filed by the permit applicant or any of the parties listed below must be filed within fourteen days of receipt of this notice of intent. Petitions filed by any persons other than those entitled to written notice under Section 120.60(3), F.S. must be filed within fourteen days of publication of the public notice or within fourteen days of receipt of this notice of intent, whichever occurs first. Under Section 120.60(3), F.S., however, any person who asked the Department for notice of agency action may file a petition within fourteen days of receipt of that notice, regardless of the date of publication. A petitioner shall mail a copy of the petition to the applicant at the address indicated above at the time of filing. The failure of any person to file a petition within the appropriate time period shall constitute a waiver of that person's right to request an administrative determination (hearing) under Sections 120.569 and 120.57, F.S. or to intervene in this proceeding and participate as a party to it. Any subsequent intervention will be only at the approval of the presiding officer upon the filing of a motion in compliance with Rule 28-106.205, F.A.C.

A petition that disputes the material facts on which the Department's action is based must contain the following information: (a) The name and address of each agency affected and each agency's file or identification number, if known; (b) The name, address, and telephone number of the petitioner, the name, address, and telephone number of the petitioner's representative, if any, which shall be the address for service purposes during the course of the proceeding; and an explanation of how the petitioner's substantial interests will be affected by the agency determination; (c) A statement of how and when petitioner received notice of the agency action or proposed action; (d) A statement of all disputed issues of material fact. If there are none, the petition must so indicate; (e) A concise statement of the ultimate facts alleged, including the specific facts the petitioner contends warrant reversal or modification of the agency's proposed action; (f) A statement of the specific rules or statutes the petitioner contends require reversal or modification of the agency's proposed action; and (g) A statement of the relief sought by the petitioner, stating precisely the action petitioner wishes the agency to take with respect to the agency's proposed action.

A petition that does not dispute the material facts upon which the Department's action is based shall state that no such facts are in dispute and otherwise shall contain the same information as set forth above, as required by Rule 28-106.301, F.A.C.

Because the administrative hearing process is designed to formulate final agency action, the filing of a petition means that the Department's final action may be different from the position taken by it in this notice. Persons whose substantial interests will be affected by any such final decision of the Department on the application have the right to petition to become a party to the proceeding, in accordance with the requirements set forth above.

A complete project file is available for public inspection during normal business hours, 8:00 a.m. to 5:00 p.m., Monday through Friday, except legal holidays, at Florida Department of Environmental Protection, South District, 2295 Victoria Avenue, Suite 364, Fort Myers, Florida and at the Division of Environmental Science and Engineering, Palm Beach County Health Department, 901 Evernia Street, West Palm Beach, Florida 33401.

The complete project file includes the application, technical evaluations, Draft permit, and the information submitted by the responsible official, exclusive of confidential records under Section 403.111, F.S. Interested persons may contact the District's Air Program Administrator or the project engineer, at 2295 Victoria Avenue, Suite 364, Fort Myers or call 239/332-6975, for additional information.



Department of Environmental Protection

Jeb Bush Governor South District P.O. Box 2549 Fort Myers, Florida 33902-2549

Colleen M. Castille Secretary

PERMITTEE:

Okeelanta Corporation Okeelanta Sugar Mill and Refinery 21250 U. S. Highway 27 South Bay, Florida 33493 Facility I.D. No.: 0990005

Permit Number: 0990005-015-AC

Date of Issue: **DRAFT**Expiration Date: **DRAFT**County: Palm Beach
Latitude: 26° 34' 39" N
Longitude: 80° 44' 58" W

Project: Modification of Construction Permits 0990005-010-AC and 0990005-013-AC

This permit is issued under the provisions of Chapter 403, Florida Statutes (F.S.), and Florida Administrative Code (F.A.C.) Rules 62-4, 62-296, and 62-297. The above named permittee is hereby authorized to perform the work or operate the facility shown on the application and approved drawing(s), plans, and other documents, attached hereto or on file with the Department and made a part hereof and specifically described as follows:

The permit modifies Construction Permit 0990005-010-AC to increase the permitted capacity of paint and thinner usage from 2,475 gallons per year to 4,950 gallons per year, modifies Construction Permit 0990005-013-AC to remove the RACT (reasonable available control technology) requirements, and then combines the permits. The paint booth has the potential to emit 0.35 tons per year of particulate matter (PM), 0.35 tons per year of PM10, 9.38 tons/year of volatile organic compound (VOC) and 0.47 tons per year of Hazardous Air Pollutants (HAPs).

The facility is located approximately six miles south of South Bay, Palm Beach County.

Pertinent Documents

Construction Application
Construction Permit 0990005-010-AC
Construction Permit 0990005-013-AC
Operating Permit 0990005-012-AV
Construction Application
Request for Additional Information request
Request for Additional Information request
2nd Request for Additional Information received

Dated

July 6, 2001 August 22, 2001 November 13, 2003 March 18, 2004 February 11, 2005 March 16, 2005 April 20, 2005 May 11, 2005 May 25, 2005

Page 1 of 4
"More Protection, Less Process"

Facility I.D. No.: 0990005

Permit Number: 0990005-015-AC

Date of Issue: **DRAFT** Expiration Date: **DRAFT**

SPECIFIC CONDITIONS:

This permit addresses the following emissions unit:

E.U.

ID No. Emissions Unit Description

048 Paint Booth

This emissions unit consists of a paint spray booth used to re-paint farm equipment used in agricultural fields, trailers for the delivery of cane to the mill, as well as other vehicles. The paint spray booth is manufactured by AFC, Inc., the drive-thru model of the Crossflo Truck spray booth, Model Number TSD6036.

- 1. <u>Permitted Capacity.</u> The maximum throughput rate of paint and thinner shall not exceed 4,950 gallons in any consecutive 12-month period. [Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.; and Applicant's Request dated February 11, 2005]
- 2. Method of Operation. Paint shall only be applied to facility owned agricultural equipment, trailers, and other vehicles. Paint will be applied by one of two methods, compressed air spray gun, or an airless paint sprayer. The compressed air spray gun will use house air within a pressure range of 60 to 80 pounds per square inch (psi). The airless paint sprayer will be a Titan airless paint sprayer, Model Epic 1100HPX. It will operate at a pressure of approximately 3,200 psi. There are two exhaust stacks for the paint spray booth. Both are 25.7 feet tall with a 4-foot diameter and have a flowrate of 45,500 acfm. [Construction Permit 0990005-010-AC, dated August 22, 2001]
- 3. <u>Hours of Operation.</u> This emissions unit is allowed to operate continuously, 8,760 hours/year. [Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.; and Construction Permit 0990005-010-AC, dated August 22, 2001]
- 4. The permittee shall not cause, suffer, allow, or permit the discharge of air pollutants which cause or contribute to an objectionable odor. [Rule 62-296.320(2), F.A.C. and Construction Permit 0990005-010-AC, dated August 22, 2001]
- 5. The permittee shall take all reasonable precautions to prevent emissions of unconfined particulate matter. The permittee shall not cause, let, permit, suffer or allow the emissions of unconfined particulate matter from any activity, including vehicular movement; transportation of materials; construction, alteration, demolition or wrecking; or industrially related activities such as unloading, storing or handling; without taking reasonable precautions to prevent such emissions. Reasonable precautions may include, but shall not be limited to,
 - (a) removal of particulate matter from roads and other paved areas under the control of the permittee, and from buildings or work areas to prevent particulate from becoming airborne,
 - (b) landscaping or planting of vegetation,
 - (c) use of hoods, fans, filter, and similar equipment to contain, capture and/or vent particulate matter, and
- (d) confining abrasive blasting and sanding where possible. [Rule 62-296.320(4)(c), F.A.C. and Construction Permit 0990005-010-AC, dated August 22, 2001]

Facility I.D. No.: 0990005

Permit Number: 0990005-015-AC

Date of Issue: **DRAFT**Expiration Date: **DRAFT**

SPECIFIC CONDITIONS:

6. All equipment, pipes, hoses, lids, fittings, etc., shall be operated/maintained in such a manner as to minimize leaks, fugitive emissions, and spills of solvent materials.

[Rule 62-296.320, F.A.C. and Construction Permit 0990005-010-AC, dated August 22, 2001]

7. The permittee may adjust the amounts and types of coatings used as necessary to comply with the conditions of this permit.

[Construction Permit 0990005-013-AC, dated November 13,2003]

8. Both paint spray booth exhaust stacks shall be equipped with functional glass fiber paint arrestor pads.

[Construction Permit 0990005-010-AC, dated August 22, 2001]

Emission Limitations and Standards

- 9. Volatile organic compounds (VOCs) emissions shall not exceed 9.38 tons per year. [Applicant's Request dated February 11, 2005]
- 10. Hazardous air pollutants (HAPs) emissions shall not exceed 0.47 tons per year. [Applicant's Request dated February 11, 2005]
- 11. Particulate matter (PM) emissions are estimated to be 0.35 tons per year. [Applicant's Request dated February 11, 2005]
- 12. Visible emissions from the paint spray booth shall not exceed 20% opacity. [Rule 62-296.320, F.A.C. and Construction Permit 0990005-010-AC, dated August 22, 2001]

Record Keeping and Reporting Requirements

- 13. The permittee shall record and maintain records of the following:
 - a) the number of hours that the spray booth is in use (actual);
 - b) the dates of operation;
 - c) the amounts and types of coatings used;
 - d) a monthly inventory of the volatile organic compounds, hazardous air pollutants and solvents used in the spray booth.

The permittee shall calculate the volatile organic compounds (VOC) emitted on a monthly basis by assuming that all VOC in the coatings and cleanup solvents are evaporated. The permittee shall calculate the hazardous air pollutants (HAP) on a monthly basis. The mass fraction of VOC and HAP from each coating material (and cleanup solvents) shall be determined from the Material Safety Data Sheets (MSDS) supplied from the vendors. The permittee shall maintain a file of MSDS for each raw material which indicates the composition of the VOCs and HAPs. Raw materials include, but are not limited to, powder coatings, solvent coatings, thinners, and cleaners. The file must be maintained on site and made available for inspection upon request. The permittee shall have until the 15th day of the following month to complete these records.

[Rules 62-210.370 and 62-4.070(3), F.A.C. and Construction Permit 0990005-013-AC, dated November 13, 2003]

PERMITTEE:

Okeelanta Corporation

Okeelanta Sugar Mill and Refinery

Facility I.D. No.: 0990005

Permit Number: 0990005-015-AC

Date of Issue: **DRAFT** Expiration Date: **DRAFT**

SPECIFIC CONDITIONS:

14. The amounts and types of coatings used and the calculated VOC and HAP emissions shall be included in the annual report.

[Rules 62-210.370 and 62-4.070(3), F.A.C. and Construction Permit 0990005-013-AC, dated November 13, 2003]

15. Copies of all reports, tests, notifications or other submittals required by this permit shall be submitted to both the Department of Environmental Protection, South District and the Palm Beach County Public Health Unit.

[Rule 62-210.370, F.A.C., and Construction Permit 0990005-010-AC dated August 22, 2001]

Reasonable Assurances

16. Issuance of this permit does not relieve the permittee of an emissions unit from complying with any applicable requirements, any emission limiting standards or other requirements of the air pollution rules of the Department or any other requirements under federal, state or local law. [Rule 62-210.300, F.A.C., and Construction Permit 0990005-010-AC dated August 22, 2001]

17. Special Compliance Tests. When the Department, after investigation, has good reason (such as complaints, increased visible emissions or questionable maintenance of control equipment) to believe that any applicable emission standard contained in a Department rule or in a permit issued pursuant to those rules is being violated, it shall require the owner or operator of the emissions unit to conduct compliance tests which identify the nature and quantity of pollutant emissions from the emissions unit and to provide a report on the results of said tests to the Department.

[Rule 62-297.310(7)(b), F.A.C. and Construction Permit 0990005-010-AC dated August 22, 2001]

General Conditions:

18. An integral part of this permit is the attached 15 General Conditions. [Rule 62-4.160, F.A.C.]

NOTE: In the event of an emergency the permittee shall contact the Department by calling (850) 413-9911. During normal business hours, the permittee shall call (239) 332-6975.

Issued this day of

2005.

STATE OF FLORIDA DEPARTMENT OF ENVIRONMENTAL PROTECTION

DRAFT

Jon M. Iglehart
Director of
District Management
Post Office Box 2549
Fort Myers, Florida 33902-2549
(239) 332-6975

JMI/DLN/iw

Facility I.D. No.: 0990005

Permit Number: 0990005-015-AC

Date of Issue: DRAFT Expiration Date: DRAFT

GENERAL CONDITIONS:

1. The terms, conditions, requirements, limitations, and restrictions set forth in this permit are "Permit Conditions" and are binding and enforceable pursuant to Sections 403.161, 403.727, or 403.859 through 403.861, Florida Statutes. The permittee is placed on notice that the Department will review this permit periodically and may initiate enforcement action for any violation of these conditions.

- 2. This permit is valid only for the specific processes and operations applied for and indicated in the approved drawings or exhibits. Any unauthorized deviation from the approved drawings or exhibits, specifications, or conditions of this permit may constitute grounds for revocation and enforcement action by the Department.
- 3. As provided in Subsections 403.087(6) and 403.722(5), Florida Statutes, the issuance of this permit does not convey any vested rights or any exclusive privileges. Neither does it authorize any injury to public or private property or any invasion of personal rights, nor any infringement of federal, state, or local laws or regulations. This permit is not a waiver or approval of any other Department permit that may be required for other aspects of the total project which are not addressed in the permit.
- 4. This permit conveys no title to land or water, does not constitute State recognition or acknowledgment of title, and does not constitute authority for the use of submerged lands unless herein provided and the necessary title or leasehold interests have been obtained from the State. Only the Trustees of the Internal Improvement Trust Fund may express State opinion as to title.
- 5. This permit does not relieve the permittee from liability for harm or injury to human health or welfare, animal, or plant life, or property caused by the construction or operation of this permitted source, or from penalties therefore; nor does it allow the permittee to cause pollution in contravention of Florida Statutes and Department rules, unless specifically authorized by any order from the Department.
- 6. The permittee shall properly operate and maintain the facility and systems of treatment and control (and related appurtenances) that are installed or used by the permittee to achieve compliance with the conditions of this permit, as required by Department rules. This provision includes the operation of backup or auxiliary facilities or similar systems when necessary to achieve compliance with the conditions of the permit and when required by Department rules.
- 7. The permittee, by accepting this permit, specifically agrees to allow authorized Department personnel, upon presentation of credentials or other documents as may be required by law and at a reasonable time, access to the premises, where the permitted activity is located or conducted to:
 - (a) Have access to and copy any records that must be kept under the conditions of the permit;
 - (b) Inspect the facility, equipment, practices, or operations regulated or required under this permit, and,
 - (c) Sample or monitor any substances or parameters at any location reasonably necessary to assure compliance with this permit or Department rules.

Facility I.D. No.: 0990005

Permit Number: 0990005-015-AC

Date of Issue: **DRAFT**Expiration Date: **DRAFT**

GENERAL CONDITIONS:

Reasonable time may depend on the nature of the concern being investigated.

- 8. If, for any reason, the permittee does not comply with or will be unable to comply with any condition or limitation specified in this permit, the permittee shall immediately provide the Department with the following information:
 - (a) A description of and cause of non-compliance; and
 - (b) The period of noncompliance, including dates and times; or, if not corrected, the anticipated time the noncompliance is expected to continue, and steps being taken to reduce, eliminate, and prevent recurrence of the non-compliance.

The permittee shall be responsible for any and all damages which may result and may be subject to enforcement action by the Department for penalties or revocation of this permit.

- 9. In accepting this permit, the permittee understands and agrees that all records, notes, monitoring data and other information relating to the construction or operation of this permitted source which are submitted to the Department may be used by the Department as evidence in any enforcement case involving the permitted source arising under the Florida Statutes or Department rules, except where such use is prescribed by Sections 403.73 and 403.111, Florida Statutes. Such evidence shall only be used to the extent it is consistent with the Florida Rules of Civil Procedure and appropriate evidentiary rules.
- 10. The permittee agrees to comply with changes in Department rules and Florida Statutes after a reasonable time for compliance, provided, however, the permittee does not waive any other rights granted by Florida Statutes or Department rules.
- 11. This permit is transferable only upon Department approval in accordance with Florida Administrative Code Rules 62-4.120 and 62-730.300, F.A.C. as applicable. The permittee shall be liable for any non-compliance of the permitted activity until the transfer is approved by the Department.
- 12. This permit or a copy thereof shall be kept at the work site of the permitted activity.
- 13. This permit incorporates the following previously issued determinations:
 - (a) Determination of Best Available Control Technology (not applicable);
 - (b) Determination of Prevention of Significant Deterioration (not applicable); and
 - (c) Compliance with New Source Performance Standards (not applicable).

Facility I.D. No.: 0990005

Permit Number: 0990005-015-AC

Date of Issue: **DRAFT**Expiration Date: **DRAFT**

GENERAL CONDITIONS:

14. The permittee shall comply with the following:

- (a) Upon request, the permittee shall furnish all records and plans required under Department rules. During enforcement actions, the retention period for all records will be extended automatically unless otherwise stipulated by the Department.
- (b) The permittee shall hold at the facility or other location designated by this permit records of all monitoring information (including all calibration and maintenance records and all original strip chart recordings for continuous monitoring instrumentation) required by the permit, copies of all reports required by this permit, and records of all data used to complete the application or this permit. These materials shall be retained at least three years from the date of the sample, measurement, report, or application unless otherwise specified by Department rule.
- (c) Records of monitoring information shall include:
 - 1. The date, exact place, and time of sampling or measurements;
 - 2. The person responsible for performing the sampling or measurements;
 - 3. The date's analyses were performed;
 - 4. The person responsible for performing the analyses;
 - 5. The analytical techniques or methods used; and
 - 6. The results of such analyses.
- 15. When requested by the Department, the permittee shall within a reasonable time furnish any information required by law, which is needed to determine compliance with the permit. If the permittee becomes aware that relevant facts were not submitted or were incorrect in the permit application or in any report to the Department, such facts or information shall be corrected promptly.

COMPLIANCE ASSURANCE MONITORING PLAN (CAM PLAN)

for

Okeelanta Corporation

Okeelanta Sugar Mill and New Hope Power Partnership Cogeneration Facilities

December 2005

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1.0 EMISSION UNITS REQUIRING CAM PLANS

1.1 CAM Rule Applicability Definition

On October 24, 2000, the Florida Department of Environmental Protection (FDEP) issued the initial Title V air operation permit (Permit No. 0990005-003-AV) to Okeelanta Corporation (Okeelanta) for the operation of the Okeelanta sugarcane processing and sugar refining operations and the adjacent New Hope Power Partnership's (NHPP's) power generation operations. The permit was revised on March 18, 2004, and issued as Permit No. 0990005-012-AV. This permit expires on October 24, 2005, and the renewal application is due to FDEP by April 24, 2005.

As part of the Title V renewal application, a Compliance Assurance Monitoring (CAM) Plan must be submitted as required by regulations adopted in Title 40, Part 64 of the Code of Federal Regulations (40 CFR 64). This regulation has been incorporated by reference in Rule 62-204.800, Florida Administrative Code (F.A.C.), and implemented in Rule 62-213.440, F.A.C.

CAM Plans are required for all Title V permitted emissions units using control devices to meet federally enforceable emission limits or standards, and that have pre-control emissions greater than "major" source thresholds. The term "major" is defined as in the Title V regulations (40 CFR 70), but applied on a source-by-source basis. For most non-hazardous pollutants, the major source threshold is 100 tons per year (TPY). For hazardous air pollutants (HAPs), the threshold is 10 TPY for an individual HAP, and 25 TPY for total HAPs combined.

The CAM Rules contain specific exemptions from applicability of the CAM Rule. Specifically exempted from the CAM Rule are emission limitations or standards promulgated under Stratospheric Ozone Regulations contained in 40 CFR 82, the Acid Rain Program contained in 40 CFR 72, or that are part of an emissions cap included in the Title V Permit. Also exempt are emission limitations or standards proposed after November 15, 1990, under New Source Performance Standards (NSPS) contained in 40 CFR 60, and National Emission Standards for Hazardous Air Pollutants (NESHAPs) promulgated in 40 CFR 63, as these limitations and standards have equivalent monitoring requirements included as part of the standard.

Inherent process equipment (IPE), or equipment that may have the effect of controlling emissions but is installed for the primary purpose of product recovery or raw material recovery, is also exempt from CAM (40 CFR 64.1). In addition, CAM does not apply to any emission limit or standard for which the Title V permit specifies a continuous compliance determination method [40 CFR 64.2(b)(1)(vi)],

provided that the method does not include an assumed control device emission reduction factor that could be affected by the actual operation and maintenance of the control device.

1.2 Emissions Units Requiring CAM Plans

A review of emissions units at the Okeelanta sugar mill and sugar refinery, including packaging and transshipment activities, and NHPP's cogeneration facility, was conducted to determine the applicability of the CAM Rule. This evaluation was conducted for each emissions unit and regulated pollutant. First, the existence of a "control device" as defined by the CAM Rule was determined on a source-by-source basis for each pollutant. Those emissions units without control devices were eliminated from further consideration. The remaining emissions units were then evaluated on a pollutant-by-pollutant basis to determine if a control device was used to meet a federally enforceable emission limit or standard.

Each pollutant without a federally enforceable emission limit or standard, emitted from a given emissions unit, was eliminated from further consideration. Uncontrolled annual emissions were then calculated for each remaining source-pollutant combination. If uncontrolled emissions for a pollutant emitted from a given emissions unit were below major source thresholds, as defined by the CAM Rule, that pollutant was not further considered.

A summary of the results of this evaluation process is presented in Table 1. Supporting information is presented in Tables 2 through 6. Specific exemptions to the applicability of the CAM Rule were also considered in this evaluation.

Each pollutant-specific emissions unit at Okeelanta Sugar Mill and NHPP, and its applicability to CAM is described below.

1.2.1 Okeelanta Mill Boiler No. 16

Okeelanta operates Boiler No. 16 at the Okeelanta sugar mill, which is a Babcock and Wilcox Model No. FM 120-97 package boiler with a maximum steam production rate of 150,000 pounds per hour (lb/hr) (24-hour average). Boiler No. 16 has a maximum heat input rate of 211 million British thermal units per hour (MMBtu/hr) when firing natural gas and 202 MMBtu/hr when firing very low sulfur distillate oil.

The only control device Boiler No. 16 has is the flue gas recirculation (FGR) system, which controls nitrogen oxides (NO_x) emissions. The boiler has emission limits set for carbon monoxide (CO) and

NO_x. Emissions of CO are not controlled by any control device, and therefore a CAM Plan for CO is not required. Since NO_x is controlled by a control device and as presented in Table 2, uncontrolled NO_x emissions are more than the major source threshold of 100 TPY, NO_x was initially determined to be a pollutant that requires CAM. However, Boiler No. 16 has a continuous emission monitoring system (CEMS), per Specific Condition No. A.10 of Permit No. 0090005-012-AV, to measure and record the emissions of NO_x from the boiler and demonstrate compliance with the CEMS. The CAM Rule contained in 40 CFR 64 specifies that emission limitations or standards for which a Part 70 or 71 permit specifies a continuous compliance demonstration method are exempt from the requirements of CAM [40 CFR 64.2(b)(1)(vi)]. Therefore, a CAM Plan for NO_x is not required.

1.2.2 Okeelanta Sugar Transshipment Facility

The Transshipment Facility at the Okeelanta sugar mill consists of multiple emissions units: the vacuum system baghouse (EU 018), the packaging lines baghouse (EU 019), the grinder baghouse (EU 20), three Sugar Silo baghouses (EUs 026, 027, and 028), the powdered sugar dryer/cooler baghouse (EU 045), the powdered sugar hopper baghouse (EU 046), and the new packaging lines baghouse (EU 047). These emission points are control devices to reduce the potential total particulate matter (PM) emissions from the facility. Maximum throughput rate of the facility is 865 tons of refined sugar per day.

Each emissions unit at the Transshipment Facility has a control device and a federally enforceable emission limit for PM in tons per year. As shown in Table 1, none of the Transshipment Facility sources (EUs 018, 019, 020, 026, 045, 046, and 047) is required to have a CAM Plan. The justification for this conclusion for each emissions unit is presented below.

The Central Vacuum System (EU 018) is designed to allow manual pickup of sugar dust from a number of pickup points located throughout the facility as needed. Based on engineering judgment, it is assumed that the amount of dust picked up by the Central Vacuum System does not exceed 100 TPY. Therefore, a CAM Plan for PM is not required for the Central Vacuum System.

Detailed descriptions of the baghouses controlling the Packaging Lines (EUs 019 and 047) and the Sugar Silos (EUs 026, 027, and 028) are provided in Attachment OC-EU2-I3 of the Title V operating permit renewal application for Okeelanta (refer to Attachment B3). Control efficiency information for the baghouses is not available as the manufacturers provided outlet grain loading without inlet grain loading information. In order to estimate the uncontrolled emission rates from these sources,

continuous or batch drop emission factors from AP-42, Section 13.2.4, were computed and used wherever appropriate.

In the Sugar Silos, bucket elevators drop sugar into the silos directly. Any air displaced by the sugar is vented through a baghouse. The "drop" equation was appropriately used to estimate uncontrolled PM/particulate matter with aerodynamic size less than 10 micrometers (PM_{10}) emissions from the sugar silos. There are a total of three sugar silos, with one transfer point per silo. However, the sugar effectively only experiences one drop since it is loaded into one of the three silos.

Similarly, the drop equation was also used to estimate uncontrolled PM and PM₁₀ emissions from the Packaging Lines. Three transfer points were used in the calculation, as the maximum number of transfer points on any packaging line is three. In reality, only one packaging line has three transfer points and all the rest have one or two points. The Packaging Lines baghouse (EU 019) controls Packaging Lines 1 through 9 and the new Packaging Lines baghouse (EU 047) controls Packaging Lines 11 through 14.

For the purpose of emissions calculation, the combined annual packaging capacity of 315,725 TPY was prorated among EUs 019 and 047 based on the number of packaging lines in each group. In all, the emissions calculations using the drop equation was used, with a refined sugar moisture content of 0.25 percent, which is the lowest rating for which the drop equation has an "A" rating. Since the transfer points are enclosed, a wind speed of 1.3 mph was used, the lowest wind speed for which the drop equation has an "A" rating.

The emissions calculations are presented in Table 3, and as demonstrated, the uncontrolled PM and PM₁₀ emissions from the Packaging Lines 1 through 9 baghouse (EU 019), Sugar Silos 1, 2, and 3 (EU 026, 027, and 028), and Packaging Lines 11 through 14 baghouse (EU 047) are less than 100 TPY. As a result, these emission units are not subject to the CAM requirements.

The Grinder (EU 020) and the Powdered Sugar Hopper (EU 046), as well as the baghouse associated with each unit, are designed in such a way that all the material from the unit either falls or is pulled into the baghouse. The baghouses act as collection mechanisms for powdered sugar and are an integral part of the process. Since these baghouses are considered part of the process, they are not considered control equipment, and as a result, the Grinder (EU 020) and the Powdered Sugar Hopper (EU 046) are not subject to the CAM requirements since they have no control device.

PM emissions from the Powdered Sugar Dryer/Cooler are controlled by a baghouse (EU 045), which is located after a cyclone. The cyclone is part of the process equipment and removes the larger PM. Based on engineering judgment, it is assumed that the sugar dust that leaves the cyclone does not exceed 100 TPY. Therefore, the powdered sugar dryer/cooler is not subject to CAM for PM.

1.2.3 Okeelanta Sugar Refinery

The Sugar Refinery unit at the Okeelanta sugar mill and refinery consists of multiple emissions units: two Central Dust Collection Systems (EU 021 and 022); the Fluidized Bed Dryer (EU 025), used as the primary sugar drying system; Cooler Nos. 1 and 2 (EU 023 and 024), used to cool dried sugar leaving the rotary dryer; the Bulk Load-out operation (EU 034), used to load sugar into either trucks or railcars; and the Transfer Bulk Load-out station (EU 035), used to supply sugar to the Transshipment Facility. Four wet rotoclones, one baghouse, and process enclosures reduce the PM emissions from the sugar refinery. Refined sugar production in the refinery is limited to 390,000 TPY and 1,500 tons per day (TPD).

EU 034 (Bulk Load-out operation) and EU 035 (Transfer Bulk Load-out operation) have no control devices and, therefore, are exempt from the CAM requirements. Each of the EUs 021, 022, 023, 024, and 025 at the sugar refinery has a control device and federally enforceable emission limits for PM and PM₁₀ on a tons-per-year basis. The derivation of uncontrolled emissions from these units is described below and summarized in Table 1.

Controlled and uncontrolled emission rates from the sugar refinery emission units are presented in Attachment OC-EU3-F1.8 of the Title V operating permit renewal application submitted with this document. Maximum emission rates for each emission unit from the three scenarios, using the rotary drying system, using the fluidized bed drying system, and using both rotary and fluidized bed drying systems, are summarized in Table 4. Uncontrolled emissions of PM or PM/PM₁₀ from the two Central Dust Collection Systems (EU 021 and 022), the Fluidized Bed Dryer (EU 025), and Cooler Nos. 1 and 2 (EU 023 and 024) are more than 100 TPY, and therefore, CAM for PM or PM/PM₁₀ is required for these units.

1.2.4 Paint Spray Booth

Okeelanta operates a paint spray booth at the sugar mill facility, which is used to repaint farm equipment that is used in the agricultural fields, trailers for the delivery of the cane to the mill, as well as other vehicles. The paint spray booth has glass fiber paint arrestor pads, which are used to reduce PM emissions.

The paint spray booth emits volatile organic compounds (VOC) and PM and has a federally enforceable emission limit for VOC. Since there are no control devices for VOC, CAM is not required for VOC. There is a control device for PM, but no emission limits. Therefore, a CAM Plan is not required for PM.

1.2.5 NHPP Cogeneration Boilers A, B, and C

Cogeneration Boilers A, B, and C at the NHPP cogeneration facility are biomass-fired spreader stoker steam boilers manufactured by Zurn and designed to produce approximately 506,100 lb/hr of steam at 1,500 pounds per square inch (psig) and 975 degrees Fahrenheit (°F). The boilers have a maximum heat input rate of 760 MMBtu/hr when firing bagasse, 605 MMBtu/hr when firing natural gas, and 490 MMBtu/hr when firing very low sulfur distillate oil.

The boilers have several control devices: a selective non-catalytic reduction system (SNCR) to reduce NO_x emissions, mechanical dust collectors and an electrostatic precipitator (ESP) to reduce PM emissions, and an activated carbon injection system to reduce potential mercury (Hg) emissions. Each of the boilers is also subject to federally enforceable emission limits for CO, NO_x, sulfur dioxide (SO₂), PM/PM₁₀, VOC, Hg, and lead (Pb). Note that the mercury control system is currently inactive and is only required to be operated in the event that the Hg emissions limit for the cogeneration boilers is exceeded. Since CO, SO₂, and VOC emissions are not controlled by any control devices, these pollutants are exempt from the requirements of CAM. As shown in Table 1, and described below, uncontrolled PM and NO_x emissions are greater than 100 TPY.

Uncontrolled NO_x, PM/PM₁₀, Hg, and Pb emissions from the NHPP boilers are estimated in Table 5. Annual emissions were calculated using the alternative fuel usage scenarios: 100-percent biomass (wood or bagasse), 75.1-percent biomass and 24.9-percent fuel oil, and 75.1-percent biomass and 24.9-percent natural gas. Uncontrolled emission factors based on fuel analysis or AP-42 were used in the calculations. In the combination fuel scenarios involving biomass and fuel oil or natural gas, the worst-case emission factors for either bagasse or wood combustion were used for each pollutant.

Since NO_x is controlled by a control device and uncontrolled NO_x emissions are more than the major source threshold of 100 TPY, NO_x was initially determined to be a pollutant that requires CAM. However, each of the cogeneration boilers has a continuous emission monitoring system (CEMS), per Specific Condition No. F.6 of Permit No. 0090005-012-AV, to measure and record the emissions of NO_x from the boiler and demonstrate compliance with the NO_x CEMS. The CAM Rules contained in 40 CFR 64 specify that emission limitations or standards for which a Part 70 or 71

permit specifies a continuous compliance demonstration method are exempt from the requirements of CAM [40 CFR 64.2(b)(1)(vi)]. Therefore, a CAM Plan for NO_x is not required for each of the cogeneration boilers.

PM/PM₁₀ emissions from each of the Boilers A, B, and C are controlled by an ESP and the uncontrolled emissions are more than the major source threshold of 100 TPY. Therefore, CAM is required for PM/PM₁₀. Boilers A, B, and C are subject to the federal NESHAPs for Industrial, Commercial, and Institutional Boilers and Process Heaters, 40 CFR 63, Subpart DDDDD, which was promulgated on September 13, 2004. The compliance date for existing sources is September 13, 2007. The Subpart DDDDD rules regulate PM emissions from existing large solid fuel boilers. The CAM Rules contained in 40 CFR 64 specify that emission limitations or standards proposed by the Administrator after November 15, 1990, pursuant to Part 111 or 112 of the Clean Air Act (CAA), are exempt from the requirements of CAM [40 CFR 64.2(b)(1)(i)]. However, there are currently no emission limits applicable to the boilers due to Subpart DDDDD, and therefore, the boilers are not exempt from CAM for PM/PM₁₀.

As shown in Table 1, uncontrolled Pb and Hg emissions from each of the Boilers A, B, and C are less than the major source threshold of 100 TPY. As a result, CAM is not required for Pb and Hg.

1.2.6 NHPP Materials Handling and Storage Operations

The materials handling and storage operations at the NHPP cogeneration facility include truck and railcar unloading operations, storage piles, transfer operations, conveyors, screens, crushers, hoppers and silos for handling and storing biomass (bagasse and wood), ash (fly and bottom), and a mercury removal agent (carbon). Baghouse control devices are used for controlling PM emissions from the fly ash and mercury control agent silos. Note that the mercury control system is currently inactive and is only required to be operated in the event that the Hg emissions limit for the cogeneration boilers is exceeded.

The fly ash and mercury control agent silos have federally enforceable emission limits for PM. As shown in Table 6, the uncontrolled PM emissions from the fly ash silo are less than 100 TPY, and therefore are not subject to the CAM Plan requirements. Similarly, uncontrolled PM emissions from the mercury removal agent silo are also less than 100 TPY; therefore, CAM is not required for the Hg control agent silo.

2.0 PM EMISSIONS FROM THE CENTRAL DUST COLLECTION SYSTEM NO. 1 (WET ROTOCLONE NO. 1) (EU 021)

2.1 Emissions Unit Identification

Central Dust Collection System No. 1 (from rotary dryer and transfer points)—EU ID No. 021

2.2 Applicable Regulations, Emissions Limits, and Monitoring Requirements

The Central Dust Collection System No. 1, which collects dust from the rotary dryer and various transfer points, is included in the overall sugar refinery PM emission limit of 36.8 TPY and 13.39 TPY PM₁₀ [Permit No. 0990005-005-AC]. The individual maximum allowable emissions from the Central Dust Collector System No. 1 are 4.13 TPY of PM and 1.65 TPY of PM₁₀. The current visible emission (VE) limit is 5-percent opacity (6-minute average). Refined sugar production is limited to 390,000 TPY.

FDEP has waived the PM compliance test requirements and has specified the alternative standard of 5-percent opacity as the method for demonstrating compliance. Okeelanta is required to monitor and record the date, amount of sugar processed through the facility and through rotary and fluidized dryer beds, amount of sugar loaded out, and hours of operation on a daily basis.

2.3 Control Technology Description

PM emissions from the Central Dust Collection System No. 1 are controlled by an American Air Filter Type W wet rotoclone (Rotoclone No. 1). A detailed description of the control equipment is included in the Title V renewal application, Attachment OC-EU3-I3 (see Attachment B).

2.4 Monitoring Approach

The monitoring approach is based on the water injection rate to the wet rotoclone. The monitoring approach is summarized in the table below.

	Indicator No. 1
Indicator	Water injection rate to the wet rotoclone.
Measurement Approach	The water injection rate is measured using a flow rate sensor.
Indicator Range	An excursion is defined as any daily average water injection rate
	below 2 gpm. Excursions trigger an inspection, corrective
4	action, and a recordkeeping and reporting requirement.
Data Representativeness	The water injection rate sensor is located on the water supply
·	line.
Verification of Operational	N/A
Status	
QA/QC Practices and Criteria	The flow rate sensor is maintained in accordance with the
	manufacturer's recommendations.
Monitoring Frequency	Water flow rate is monitored once every day in a log.
Data Collection Procedures	Water flow rate data is recorded once every day.
Averaging Period	N/A

2.5 <u>Justification</u>

Both pressure drop across and water injection rate to the wet rotoclone are recognized parameters for controlling PM emissions from wet rotoclones. The pressure drop is a measure of the energy imparted to the gas stream and, therefore, the efficiency of the control process. The water injection rate is a measure of sufficient fresh water being supplied to the rotoclone and also relates to the efficiency of control. However, measuring the pressure drop continually in the rotoclones has proven to be impractical due to fouling in the instrument sample lines. Therefore, Okeelanta is requesting in the Title V permit renewal application that the pressure drop column be deleted in the construction restrictions conditions of Subsection D of Permit No. 0090005-012-AV. Okeelanta is proposing to monitor the water injection rate to the rotoclone for the purpose of assuring compliance with the PM emission standard.

The operating ranges are based on the design information and the efficiency ratings provided by the manufacturer, as well as the values experienced during the 2004 stack testing of the Rotoclone No 1. The design parameters are provided in Attachment B. VE test results for the Rotoclone No. 1 are also included in Attachment B. The VE test results conducted during normal operation of the Wet Rotoclone No. 1 demonstrated that opacity from the Rotoclone No. 1 stack is less than 5 percent, which is also the alternative standard for demonstrating compliance with the PM standard. This

shows that monitoring during normal operation of the rotoclone can assure compliance with the PM standard.

When an excursion occurs, corrective action will be initiated, beginning with an evaluation of the occurrence, to determine the action required (if any) to correct the situation. All excursions will be documented and reported.

3.0 PM EMISSIONS FROM THE CENTRAL DUST COLLECTION SYSTEM NO. 2 (WET ROTOCLONE NO. 2) (EU 022)

3.1 Emissions Unit Identification

Central Dust Collection System No. 2—EU ID No. 022

3.2 Applicable Regulations, Emissions Limits, and Monitoring Requirements

The Central Dust Collection System No. 2 is included in the overall sugar refinery PM emission limit of 36.8 TPY and 13.39 TPY PM₁₀ [Permit No. 0990005-005-AC]. The individual maximum allowable emissions from the Central Dust Collector System No. 2 are 0.18 TPY of PM and 0.073 TPY of PM₁₀. The current VE limit is 5-percent opacity (6-minute average). Refined sugar throughput of material handling is limited to 390,000 TPY.

FDEP has waived the PM compliance test requirements and has specified the alternative standard of 5-percent opacity as the method for demonstrating compliance.

3.3 Control Technology Description

PM emissions from the Central Dust Collection System No. 2 are controlled by an American Air Filter Type W wet rotoclone (Rotoclone No. 2). A detailed description of the control equipment is included in the Title V renewal application, Attachment OC-EU3-I3 (see Attachment B).

3.4 Monitoring Approach

The monitoring approach is based on water injection rate to the wet rotoclone. The monitoring approach is summarized in the table below.

	Indicator No. 1
Indicator	Water injection rate to the wet rotoclone.
Measurement Approach	The water injection rate is measured using a flow rate sensor.
Indicator Range	An excursion is defined as any daily average water injection rate below 2 gpm. Excursions trigger an inspection, corrective
	action, and a recordkeeping and reporting requirement.
Data Representativeness	The water injection rate sensor is located on the water supply
	line.
Verification of Operational	NA
Status	
QA/QC Practices and Criteria	The flow rate sensor is maintained in accordance with the
	manufacturer's recommendations.
Monitoring Frequency	Water flow rate is monitored once every day in a log.
Data Collection Procedures	Water flow rate data is recorded once every day.
Averaging Period	N/A ·

3.5 Justification

Both pressure drop across and water injection rate to the wet rotoclone are recognized parameters for controlling PM emissions from wet rotoclones. The pressure drop is a measure of the energy imparted to the gas stream and, therefore, the efficiency of the control process. The water injection rate is a measure of sufficient fresh water being supplied to the rotoclone and also relates to the efficiency of control. However, measuring the pressure drop continually in the rotoclones has proven to be impractical due to fouling in the instrument sample lines. Therefore, Okeelanta is requesting in the Title V permit renewal application that the pressure drop column be deleted in the construction restrictions conditions of Subsection D of Permit No. 0090005-012-AV. Okeelanta is proposing to monitor the water injection rate to the rotoclone for the purpose of assuring compliance with the PM emission standard.

The operating ranges are based on the design information and the efficiency ratings provided by the manufacturer, and in the values experienced during the 2004 stack testing of the Wet Rotoclone No. 2. The design parameters are provided in Attachment B. Also provided in Attachment B are the results of VE testing conducted on the rotoclone. The VE test results conducted during normal operation of the Wet Rotoclone No. 1 demonstrated that opacity from the Rotoclone No. 2 stack is less than 5 percent, which is also the alternative standard for demonstrating compliance with the PM

standard. This shows that monitoring during normal operation of the rotoclone can assure compliance with the PM standard.

When an excursion occurs, corrective action will be initiated, beginning with an evaluation of the occurrence, to determine the action required (if any) to correct the situation. All excursions will be documented and reported.

4.0 PM EMISSIONS FROM COOLER NO. 1 (WET ROTOCLONE NO. 3) (EU 023)

4.1 Emissions Unit Identification

Cooler No. 1—EU ID No. 023.

4.2 Applicable Regulations, Emissions Limits, and Monitoring Requirements

Cooler No. 1 of the rotary drying system is included in the overall sugar refinery PM emission limit of 36.8 TPY and 13.39 TPY PM₁₀ [Permit No. 0990005-005-AC]. Maximum allowable emissions from Cooler No. 1 are 10.01 TPY of PM and 5.59 TPY of PM₁₀. The current VE limit is 5-percent opacity (6-minute average). Refined sugar production is limited to 390,000 TPY.

FDEP has waived the PM compliance test requirements and has specified the alternative standard of 5-percent opacity as the method for demonstrating compliance. Okeelanta is required to monitor and record the date, amount of sugar processed through the facility and through each cooler, and hours of operation on a daily basis.

4.3 Control Technology Description

PM emissions from the rotary drying system Cooler No. 1 are controlled by an American Air Filter Type W wet rotoclone (Rotoclone No. 3). A detailed description of the control equipment is included in the Title V renewal application, Attachment OC-EU3-I3 (see Attachment B).

4.4 Monitoring Approach

The monitoring approach is based on water injection rate to the wet rotoclone. The monitoring approach is summarized in the table below.

	Indicator No. 1
Indicator	Water injection rate to the wet rotoclone.
Measurement Approach	The water injection rate is measured using a flow rate sensor.
Indicator Range	An excursion is defined as any daily average water injection rate
	below 2 gpm. Excursions trigger an inspection, corrective action,
<u> </u>	and a recordkeeping and reporting requirement.
Data Representativeness	The water injection rate sensor is located on the water supply line.
Verification of Operational	N/A
Status	
QA/QC Practices and Criteria	The flow rate sensor is maintained in accordance with the
	manufacturer's recommendations.
Monitoring Frequency	Water flow rate is monitored once every day in a log.
Data Collection Procedures	Water flow rate data is recorded once every day.
Averaging Period	N/A

4.5 Justification

Both pressure drop and water injection rate to the wet rotoclone are recognized parameters for controlling PM emissions from wet rotoclones. The pressure drop is a measure of the energy imparted to the gas stream and, therefore, the efficiency of the control process. The water injection rate is a measure of sufficient fresh water being supplied to the wet rotoclone and also relates to the efficiency of collection. However, measuring the pressure drop continually in the wet rotoclone has proven to be impractical due to fouling in the instrument sample lines. Therefore, Okeelanta is requesting in the Title V permit renewal application that the pressure drop column be deleted in the construction restriction conditions of Subsection D of Permit No. 0090005-012-AV. Okeelanta is proposing to monitor the water injection rate to the wet rotoclone for the purpose of assuring compliance with the PM emission standard.

The operating ranges are based on the design information and the efficiency ratings provided by the manufacturer. The design parameters are provided in Attachment B.

A VE compliance test will be conducted on the Rotoclone No. 3 stack in the near future and the minimum water injection rate will be set based on the test. The VE test, which will be conducted during normal operation, is also an alternative standard for demonstrating compliance with the PM standard, if opacity is under 5 percent.

When an excursion occurs, corrective action will be initiated, beginning with an evaluation of the occurrence, to determine the action required (if any) to correct the situation. All excursions will be documented and reported.

5.0 PM EMISSIONS FROM COOLER NO. 2 (WET ROTOCLONE NO. 4) (EU 024)

5.1 <u>Emissions Unit Identification</u>

Cooler No. 2-EU ID No. 024

5.2 Applicable Regulations, Emissions Limits, and Monitoring Requirements

Cooler No. 2 of the rotary drying system is included in the overall sugar refinery PM emission limit of 36.8 TPY and 13.39 TPY PM₁₀ [Permit No. 0990005-005-AC]. Maximum allowable emissions from Cooler No. 2 are 10.01 TPY of PM and 5.59 TPY of PM₁₀. The current VE limit is 5-percent opacity (6-minute average). Refined sugar production is limited to 390,000 TPY.

FDEP has waived the PM compliance test requirements and has specified the alternative standard of 5-percent opacity as the method for demonstrating compliance. Okeelanta is required to monitor and record the date, amount of sugar processed through the facility and through each cooler, and hours of operation on a daily basis.

5.3 Control Technology Description

PM emissions from the rotary drying system Cooler No. 2 are controlled by an American Air Filter Type W wet rotoclone (Rotoclone No. 4). A detailed description of the control equipment is included in the Title V renewal application, Attachment OC-EU3-I3 (see Attachment B).

5.4 Monitoring Approach

The monitoring approach is based on water injection rate to the wet rotoclone. The monitoring approach is summarized in the table below.

	Indicator No. 1
Indicator	Water injection rate to the wet rotoclone.
Measurement Approach	The water injection rate is measured using a flow rate sensor.
Indicator Range	An excursion is defined as any daily average water injection rate below 2 gpm. Excursions trigger an inspection, corrective action, and a recordkeeping and reporting requirement.
Data Representativeness	The water injection rate sensor is located on the water supply line.
Verification of Operational Status	NA .
QA/QC Practices and Criteria	The flow rate sensor is maintained in accordance with the manufacturer's recommendations.
Monitoring Frequency	Water flow rate is monitored once every day in a log.
Data Collection Procedures	Water flow rate data is recorded once every day.
Averaging Period	N/A

5.5 Justification

Both pressure drop and water injection rate to the wet rotoclone are recognized parameters for controlling PM emissions from wet rotoclones. The pressure drop is a measure of the energy imparted to the gas stream and, therefore, the efficiency of the control process. The water injection rate is a measure of sufficient fresh water being supplied to the wet rotoclone, as well as the efficiency of PM control. However, measuring the pressure drop continually in the wet rotoclone has proven to be impractical due to fouling in the instrument sample lines. Therefore, Okeelanta is requesting in the Title V permit renewal application that the pressure drop column be deleted in the construction restriction conditions of Subsection D of Permit No. 0090005-012-AV. Okeelanta is proposing to monitor the water injection rate to the wet rotoclone for the purpose of assuring compliance with the PM emission standard.

The operating ranges are based on the design information and the efficiency ratings provided by the manufacturer. The design parameters are provided in Attachment B.

A VE compliance test will be conducted on the Rotoclone No. 4 stack in the near future and the minimum water injection rate will be set based on the test. The VE test, which will be conducted

during normal operation, is also an alternative standard for demonstrating compliance with the PM standard, if opacity is under 5 percent.

When an excursion occurs, corrective action will be initiated, beginning with an evaluation of the occurrence, to determine the action required (if any) to correct the situation. All excursions will be documented and reported.

6.0 PM EMISSIONS FROM THE FLUIDIZED BED DRYER/COOLER (EU 025)

6.1 Emissions Unit Identification

Fluidized Bed Dryer/Cooler—EU ID No. 025

6.2 Applicable Regulations, Emissions Limits, and Monitoring Requirements

The Fluidized Bed Dryer/Cooler of the fluidized bed drying system is included in the overall sugar refinery PM emission limit of 36.8 TPY and 13.39 TPY PM₁₀ [Permit No. 0990005-005-AC]. The current VE limit is 5-percent opacity (6-minute average). Refined sugar production is limited to 390,000 TPY.

FDEP has waived the PM compliance test requirements and has specified the alternative standard of 5-percent opacity as the method for demonstrating compliance. Okeelanta is required to monitor and record the date, amount of sugar processed through the facility and through the rotary and fluidized bed dryers, amount of sugar loaded out, and hours of operation on a daily basis.

6.3 <u>Control Technology Description</u>

PM emissions from the fluidized bed drying system are controlled by a BETH GmbH pulse jet compressed air baghouse. A detailed description of the control equipment is included in the Title V renewal application, Attachment OC-EU3-I3 (see Attachment B).

6.4 Monitoring Approach

The monitoring approach is based on pressure drop across the baghouse. The monitoring approach is summarized in the table below.

0.40 Variable 1 - 1	Indicator No. 1						
Indicator	Pressure drop across the baghouse.						
Measurement Approach	Pressure drop is monitored with a manometer.						
Indicator Range	An excursion is defined as any daily average pressure drop value below 5 millibars, after steady-state operations have been achieved. Excursions trigger an inspection, corrective action, and a recordkeeping and reporting requirement.						
Data Representativeness	The monitoring system consists of a manometer, which measures the pressure drop across the baghouse.						
Verification of Operational Status	NA						
QA/QC Practices and Criteria	The manometer is maintained in accordance with the manufacturer's recommendations.						
Monitoring Frequency	Pressure drop is monitored once every day.						
Data Collection Procedures	Pressure drop data is recorded once every day after steady state operations have been achieved.						
Averaging Period	N/A						

6.5 Justification

Okeelanta is proposing to monitor pressure drop across the baghouse, which is a recognized parameter for controlling PM emissions from baghouses. The pressure drop is a measure of the energy imparted to the gas stream and, therefore, the efficiency of the control process. The normal operating range of pressure drop for the Fluidized Bed Dryer/Cooler baghouse is 5 to 20 millibars. Other manufacturer design information is provided in Attachment B.

A pressure drop less than 5 millibars means a broken bag or flow bypass around the bags, which would require shutdown and replacement of bags. Results of annual VE tests conducted during normal operation of the Fluidized Bed Dryer/Cooler and the associated baghouse demonstrated that opacity from the baghouse stack is less than 5 percent, which is also the alternative standard for demonstrating compliance with the PM standard. This shows that monitoring for the normal operation of the baghouse can assure compliance with the PM standard. VE test data for the Fluidized Bed Dryer/Cooler are presented in Attachment B.

When an excursion occurs, corrective action will be initiated, beginning with an evaluation of the occurrence, to determine the action required (if any) to correct the situation. All excursions will be documented and reported.

7.0 PM EMISSIONS FROM COGENERATION BOILERS A, B, AND C

7.1 Emissions Unit Identification

NHPP Cogeneration Boilers A, B, and C

7.2 Applicable Regulations, Emissions Limits, and Monitoring Requirements

Cogeneration Boilers A, B, and C at the NHPP cogeneration facility are biomass-fired spreader stoker steam boilers manufactured by Zurn and designed to produce approximately 506,100 lb/hr of steam each. Each boiler has a PM emission limit of 0.026 lb/MMBtu or 19.8 lb/hr and a NO_x emission limit of 0.15 lb/MMBtu or 114.0 lb/hr.

Compliance with the NO_x emission standard is determined by data collected by the NO_x continuous emission measurement system (CEMS) in terms of "lb/MMBtu of heat input". Compliance with the PM standard is determined by the average of three test runs conducted in accordance with U.S. Environmental Protection Agency (EPA) Method 5. Each boiler also has a stack opacity limit of 6-minute block average opacity of 20 percent, except for one 6-minute block per hour that is less than or equal to 27-percent opacity. Compliance with the opacity standard is determined by a COMS, which measures opacity continuously at 1-minute intervals.

7.3 Control Technology Description

PM emissions from each of the Boilers A, B, and C are controlled by mechanical dust collectors and an ESP. NO_x emissions are controlled by a SNCR system. A detailed description of the control equipment is included in the Title V renewal application, Attachment OC-EU5-I3 (see Attachment B).

7.4 Monitoring Approach

The monitoring approach is based on monitoring opacity of each boiler stack through the existing COMS at each stack. The monitoring approach is summarized in the table below.

The second secon	Indicator No. 1
Indicator	Opacity
Measurement Approach	Continuous opacity monitoring system (COMS).
Indicator Range	An excursion is defined as any 1-hour block average of opacity greater than 20%, excluding periods of startup, shutdown, and malfunction pursuant to Rule 62-210.700, F.A.C.
	An excursion will trigger an evaluation of operation of the boiler and ESP. Corrective action will be taken as necessary. Excursions trigger recordkeeping and reporting requirements.
Data Representativeness	Opacity measurements are made in the stack.
Verification of Operational Status	N/A .
QA/QC Practices and Criteria	Install and operate COMS according to 40 CFR Part 60 Appendix B, Performance Specification 1 and general provisions 60.13.
Monitoring Frequency	Opacity is monitored continuously.
Data Collection Procedures	One-minute averages are recorded through the DAS. Daily reports with all hourly averages are generated. One-hour block averages are determined from the average of all the valid 1-minute averages during a block hour.
Averaging Period	The averaging period for opacity observations is a 1-hour block average.

7.4.1 Justification

The CAM Rule, in 40 CFR 64.3(d)(1), states that if a COMS is required pursuant to other authority under the CAA or state or local law, the owner or operator shall use such system to satisfy the requirements of this part. NHPP is proposing to use data from the COMS at each of the Boilers A, B, and C stacks and monitor the 1-hour block average opacity to assure compliance with the PM emission standard.

The NHPP boilers are subject to CAM for PM emissions, not VE. Annual compliance tests for PM are performed via EPA Method 5 and consist of three test runs each typically exceeding 1 hour in duration each. The opacity data NHPP has used to correlate PM emissions and opacity were the

average opacity for the duration of the test run (60 minutes) (see discussion below). Therefore, a 1-hour block averaging time for the CAM opacity indicator is appropriate for compliance assurance of PM emissions. As described below, at least three other power plants in Florida have received averaging times of 1-hour block duration for their CAM Plans.

NHPP has researched other CAM Plans for PM for coal-fired power plants that also use opacity as the CAM parameter. For Cedar Bay Generating Company, FDEP issued the CAM Plan based on a 10-percent opacity reading as the level defining an excursion. This level of opacity would have to be exceeded for five consecutive 6-minute averages in order to define an excursion. The rationale stated in the CAM Plan was as follows:

"Based on available data under normal operation, the representative stack opacity of each unit is in the range of 3% to 7%. A 50% average opacity above 7% during non-startup or shutdown periods is atypical and may indicate a potential problem with the baghouse."

St. Johns River Power Park received an 18-percent opacity level as the CAM indicator, based on a 1-hour block average. The rationale stated in the CAM Plan was as follows:

"Based on available data under normal operation, the representative stack opacity of each unit is in the range of 5% to 15%. In addition, the COMS are located upstream of the scrubber, and, as such, the opacity at the stack exit is lower than the value indicated by the COMS. Therefore, 18% opacity during non-startup or shutdown periods is atypical and may indicate a potential problem with the ESP."

Lakeland McIntosh received a 12-percent opacity level as the CAM indicator, based on a 1-hour average, excluding periods of startup, shutdown, and malfunction. Indiantown Cogeneration received a 6-percent opacity level as the CAM indicator, based on a 1-hour block average, excluding startup and shutdown.

For the NHPP boilers, compliance with the PM standard is currently determined by the average of three test runs conducted in accordance with EPA Method 5. Data for the compliance test runs from 2002 through 2005 were collected and are summarized in Table C-1. Based on the opacity data from the COMS, which were also collected during the test runs, an opacity versus PM emission rate plot was generated, which is shown in Figure C-1. The plot indicates a general increase in opacity as the PM emission rate increases. Except for one observation of 5-percent opacity at 14.6 lb/hr of PM

emission, opacities of 10 to 14 percent were observed for a PM emission rate in the range of 10 to 12 lb/hr. The PM emission limit for Boilers A, B, and C is 19.8 lb/hr at 760 MMBtu/hr heat input.

The variability in opacity versus PM emission rate is typical. A sudden and sustained step-increase in opacity usually indicates a potential problem with the ESP.

Using the same rationale as for Cedar Bay Generating Company, the indicator range for the NHPP Boilers A, B, and C should be set at 50-percent greater than 14-percent opacity (i.e., at 21-percent opacity). A 50-percent average opacity above the normal range is atypical, and setting the indicator range at 50-percent greater than 14-percent opacity (i.e., at 21-percent opacity), is an appropriate range of opacity, above which may indicate potential problems with the ESP. However, Boilers A, B, and C each have a stack opacity limit of 20 percent. Therefore, the indicator range is set at a maximum of 20 percent during non-startup, shutdown, and malfunction conditions.

When an excursion occurs, corrective action will be initiated, beginning with an evaluation of the occurrence, to determine the action required (if any) to correct the situation. All excursions will be documented and reported.

TABLE 1
CAM APPLICABILITY DETERMINATION FOR OKEELANTA CORPORATION AND NEW HOPE POWER PARTNERSHIP

Emission Source	Title V EU ID	Control Equipment	Pollutants with Emission Limits	Uncontrolled Emission Rate (TPY)	CAM Plan Required? (Yes/No)	Comments
Okeelanta Mill Boller No. 16	. 014	Flue Gas Recirculation	NO _x	126.8	No	Title V permit specifies continuous compliance determination method.
		None	со		No	No control device for CO.
Okeelanta Sugar Transshipment Facility						
Central Vacuum System	. 018	Baghouse	PM	<100	No	PM uncontrolled emissions < 100 TPY.
Packaging Lines (1-9)	019	Baghouse	PM	2.5	No	PM uncontrolled emissions < 100 TPY.
Grinder	020	None	PM		No	No control device.
Sugar Silo Nos. 1, 2, and 3	026, 027, 028	Baghouse	PM	1.2	No	PM uncontrolled emissions < 100 TPY.
Powdered Sugar Dryer/Cooler	045	Baghouse	PM	<100	No	PM uncontrolled emissions < 100 TPY.
Powdered Sugar Hopper	046	None	PM		No	No control device.
Packaging Lines (11 - 14)	047	Baghouse	PM	1.1	No	PM uncontrolled emissions < 100 TPY.
Okeelanta Sugar Refinery						
Central Dust Collection System No. 1	021	Rotocione	PM	4,135.8	Yes	PM uncontrolled emissions >100 TPY.
(Wet Rotoclone No. 1)		Rotocione	PM_{10}	165.4	Yes	PM ₁₀ uncontrolled emissions >100 TPY.
Central Dust Collection System No. 2	022	Rotoclone	PM	183.4	Yes	PM uncontrolled emissions >100 TPY.
(Wet Rotoclone No. 2)		Rotoclone	PM ₁₀	7.3	No	PM ₁₀ uncontrolled emissions <100 TPY.
Cooler No. 1 / Rotoclone No. 3	023	Rotoclone	PM	227.5	Yes	PM uncontrolled emissions >100 TPY.
(Wet Rotoclone No. 3)	023	Rotoclone	PM ₁₀	9.1	No	PM ₁₀ uncontrolled emissions <100 TPY.
Cooler No. 2 / Rotoclone No. 4	024	Rotoclone	PM	227.5	Yes	PM uncontrolled emissions >100 TPY.
(Wet Rotoclone No. 4)	024	Rotoclone	PM ₁₀	9.1	No	PM ₁₀ uncontrolled emissions <100 TPY.
Fluidized Bed Dryer	025	Baghouse	PM	3,900.0	Yes	PM uncontrolled emissions >100 TPY.
·		Baghouse	PM_{10}	156.0	Yes	PM ₁₀ uncontrolled emissions >100 TPY.
Bulk Load-out Operations	034	None	PM		No	No control device.
		None	PM_{10}		No	No control device.
Transfer Bulk Load-out Operations	035	None	PM		No	No control device.
		None	PM ₁₀		No	No control device.
Okeelanta Paint Booth	048	None	VOC		No	No control device.
New Hope Power Boilers A, B, C	001, 002, 003	ESP	PM	7,223.5	Yes	PM uncontrolled emissions >100 TPY.
(each)	001, 002, 003	ESP	PM ₁₀	7,223.5	Yes	PM ₁₀ uncontrolled emissions >100 TPY.
(cacil)		SNCR	NO _x	732.3	No	Title V permit specifies continuous compliance determination method.
		None	со		No	No control device.
•		None	SO ₂	*	No	No control device.
		None	VOC		No	No control device.
		ESP	Pb	0.4	No	Pb uncontrolled emissions <100 TPY.
		Carbon Injection	Hg	0.018	No	Hg uncontrolled emissions <100 TPY.
New Hope Power Material Handling and						•
Storage Operations Fly Ash Silo	004	Baghouse	PM	93.9	No	PM uncontrolled emissions < 100 TPY.
Mercury Reagent Silo	004	Baghouse Baghouse	PM PM	93.9	No No	PM uncontrolled emissions < 100 TPY. PM uncontrolled emissions < 100 TPY.

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TABLE 2
UNCONTROLLED NOX EMISSIONS FROM BOILER NO. 16, OKEELANTA CORPORATION

		Natural Gas Combustion							
Regulated Pollutant	Emission Factor (lb/10 ⁶ scf)	Emission Factor (lb/MMBtu)	Ref.	Activity Factor ^a (MMBtu/hr)	Hourly Emissions (lb/hr)	Annual Emissions ^b (TPY)			
Nitrogen oxides (NO _x)	140	0.14	1	211	28.96	126.85			

References:

1. Factors for natural gas combustion from AP-42, Table 1.4-1 (7/98). Factors were converted to lb/MMBtu by dividing by 1,020 Btu/scf.

Footnotes:

Sample Calculations:

Hourly Emissions = Emission Factor x Activity Factor

Annual Emissions = Hourly Emissions x hours of operation (hrs/yr) / 2,000 (lb/ton)

^a The maximum permitted heat input rate is 211 MMBtu/hr for natural gas and 202 MMBtu/hr for fuel oil.

^b Based on maximum operation of 8,760 hours.

TABLE 3
UNCONTROLLED PM EMISSIONS FROM THE TRANSSHIPMENT FACILITY

Source	Control Device	Point Point ID	Type of Operation ^a	M Moisture Content (%)	U Wind Speed ^b (MPH)	Uncontrolled PM Emission Factor (lb/ton)	Annual Activity Factor ^c (TPY)	No. of Drop Points	Maximum Uncontrolled Annual PM Emissions (tons/yr)
Packaging Lines (1-9)	Baghouse	019	CONTINUOUS DROP	0.25	1.3	0.00755	218,579	3	2.5
Sugar Silo No. 1, 2, and 3	Baghouse	026, 027, 028	CONTINUOUS DROP	0.25	1.3	0.00755	315,725	1	1.2
Packaging Lines (11 - 14)	Baghouse	047	CONTINUOUS DROP	0.25	1.3	0.00755	97,146	3	1.1

Notes/References:

^a Continuous Drop Emission Factors are computed from AP-42 (USEPA, 1995) Section 13.2.4:

E= k x 0.0032 x $(U/5)^{1.3}$ / $(M/2)^{1.4}$ lb/ton, where k = 0.74 for PM.

^b Since the transfer points are enclosed, a wind speed of 1.3 mph was used for which the equation maintains an "A" quality rating.

^c Based on 865 tons/day sugar production, permit condition in permit No. 0990005-012-AV. Total throughput prorated through packaging lines based on number of lines.

TABLE 4
ANNUAL AND SHORT TERM UNCONTROLLED PARTICULATE MATTER EMISSIONS FROM OKEELANTA SUGAR REFINERY
USING THE COMBINATION OF THE FLUIDIZED BED DRYING SYSTEM AND THE ROATRY DRYING SYSTEM

Source Emission	Refined Sugar Emission Throughput				PM Uncontrolled Emission	Uncontrolled PM Emissions	
Point Description	Unit ID No.	(TPD)	(TPD) (lb/hr)		Factor	(TPY)	
	rticulate Matter (PM)					
Fluidized Bed Drying System							
Fluidized Bed Baghouse	025	1,050	87,500	260,000	1.5 %	3900.0	
Rotary Drying System							
Cooler No. 1 / Wet Rotoclone No. 3	023	450	37,500	130,000	0.175 %	227.5	
Cooler No. 2 / Wet Rotoclone No. 4	024	450	37,500	130,000	0.175 %	227.5	
AAF Skimmer/Wet Rotoclone No. 1 (from dryer)	021	450	37,500	130,000	3.150 %	4095.0	
Material Handling				•			
AAF Skimmer/Wet Rotoclone No.1 (from transfer points)	021	1,500	125,000	390,000	0.2090 lb/ton	40.8	
AAF Wet Rotoclone No. 2	022	1,500	125,000	390,000	0.9407 lb/ton	183.4	
Bulk and Transfer Load-Out Operations							
Bulk Load-out Operations	034	600	88,000	117,000	0.105 lb/ton	6.1	
Transfer Bulk Load-out Operations	035	1,200	144,000	273,000	0.105 lb/ton	14.3 8694.6	
Pa	rticulate Matter <u>(</u> P	PM10)				8094.0	
Fluidized Bed Drying System			•				
Fluidized Bed Baghouse	025	1,050	87,500	260,000	0.060 %	156.0	
Rotary Drying System							
Cooler No. 1 / Wet Rotoclone No. 3	023	450	37,500	130,000	0.007 %	9.1	
Cooler No. 2 / Wet Rotoclone No. 4	024	450	37,500	130,000	0.007 %	9.1	
AAF Skimmer/Wet Rotoclone No. 1 (from dryer)	021	450	37,500	130,000	0.126 %	163.8	
Material Handling							
AAF Skimmer/Wet Rotoclone No. 1 (from transfer points)	021	1,500	125,000	390,000	0.00836 lb/ton	1.6	
AAF Wet Rotoclone No. 2	022	. 1,500	125,000	390,000	0.03763 lb/ton	7.3	
Bulk and Transfer Load-Out Operations							
Bulk Load-out Operations	034	600	88,000	117,000	0.00418 lb/ton	0.2	
Transfer Bulk Load-out Operations	035	1,200	144,000	273,000	0.00418 lb/ton	0.6	
						347.8	
Note: See Attachment OC-EU3-F1.8 of the Title V renewal a	11 6 . 6			1 1			

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TABLE 5

MAXIMUM ANNUAL UNCONTROLLED EMISSIONS PER BOILER, NEW HOPE POWER PARTNERSHIP COGENERATION FACILITY

		Biomass			Alternate Fuel	·	Total Annual	
Regulated Pollutant	Uncontrolled Emission Factor (lb/MMBtu)	Activity Factor (10 ¹² Btu/yr)	Uncontrolled Annual Emissions (TPY)	Uncontrolled Emission Factor (lb/MMBtu)	Activity Factor (10 ¹² Btu/yr)	Uncontrolled Annual Emissions (TPY)	Uncontrolled Emissions Per Boiler (TPY)	
			100% Bagasse					
Particulate (PM)	2.17 (1)	6.658	7223.5				7,223.5 °	
Nitrogen oxides	0.17 (1)	6.658	565.9				565.9	
Lead	·1.2E-04 (2)	6.658	0.399			. 	0.40 ª	
Mercury	1.3E-06 (2)	6.658	0.0043				0.004	
		•	100% Wood					
Particulate (PM)	0.56 (3)	6.658	1864.1			~-	1,864.1	
Nitrogen oxides	0.22 (3)	6.658	732.3				732.3 ^a	
Lead .	4.8E-05 (3)	6.658	0.160				0.16	
Mercury	5.4E-06 (3)	6.658	0.0180		-		0.018 ª	
			75.1% Biomass / 24.	9% Fuel Oil b				
Particulate (PM)	2.17 (1)	5.000	5424.8	0.014 (4)	1.658	11.6	5,436.45	
Nitrogen oxides	0.22 (3)	5.000	550.0	0.174 (4)	1.658	144.2	694.21	
Lead	1.2E-04 (2)	5.000	. 0.300	9.0E-06 (4)	1.658	7.46E-03	0.31	
Mercury	5.4E-06 (3)	5.000	0.0135	3.0E-06 (4)	1.658	0.0025	0.016	
			75.1% Biomass / 2	4.9% Natural Gas b				
Particulate (PM)	2.17. (1)	5.000	5424.8	0.0075 (5)	1.658	. 6.2	5,431.06	
Nitrogen oxides	0.22 (3)	5.000	550.0	0.186 (5)	1.658	154.2	704.15	
Lead	1.2E-04 (2)	5.000	0.300	4.9E-07 (5)	1.658	4.06E-04	0.30	
Mercury	5.4E-06 (3)	5.000	0.0135	2.6E-07 (5)	1.658	2.11E-04	0.014	

^a Denotes maximum annual emissions for any fuel scenario.

References

- (1) Bagasse combustion in sugar mills, AP-42, Table 1.8-1.
- (2) Fuel analysis data from sugar industry.
- (3) Wood combustion, AP-42, Tables 1.6-1, 1.6-2, and 1.6-4.
- (4) Fuel oil combustion, AP-42, Tables 1.3-1 and 1.3-10.
- (5) Natural gas combustion, AP-42, Tables 1.4-1, 1.4-2, and 1.4-4.

^b Utilizes the worst-case emission factor for either bagasse or wood.

TABLE 6
NEW HOPE POWER PARTNERSHIP COGENERATION FACILITY UNCONTROLLED EMISSIONS FROM MATERIALS HANDLING AND STORAGE OPERATIONS

			Control		itrolled	Uncontrolled			
SOURCE	Emission	Emission Factor		Activity		Emission Factor ^a		_Maximum Emissions ^b	
	PM (gr/acf)	PM ₁₀ (gr/acf)	Factor (acfm)	Control	Efficiency (%)	PM (gr/acf)	PM ₁₀ (gr/acf)	PM(TSP) (TPY)	PM ₁₀ (TPY)
Fly Ash Silo	0.01	0.00473	2,500	BAGHOUSE	99	1.0	0.473	93.9	44.4
Mercury Reagent Silo	0.01	0.00473	2,500	BAGHOUSE	99	1.0	0.473	0.11	0.05

Notes/References:

^a Back-calculated based on controlled emission rate and control efficiency used in the controlled emission rate calculation.

^b For Fly Ash silo, based on 8,760 hr/yr operation. For Mercury Reagent Silo, based on 8 lb/hr/unit usage @ 8,760 hr/yr (105 TPY total); 10 TPH loaded per truck (10 hrs/yr operating time).

ATTACHMENT A

SIGNATURE PAGES

APPLICATION INFORMATION

Pr	ofessional Engineer Certification
1.	Professional Engineer Name: David A. Buff
	Registration Number: 19011
2.	Professional Engineer Mailing Address
	Organization/Firm: Golder Associates Inc.**
	Street Address: 6241 NW 23 rd Street, Suite 500
2	City: Gainesville State: FL Zip Code: 32653
3.	Professional Engineer Telephone Numbers Telephone: (352) 336-5600 ext.545 Fax: (352) 336-6603
4.	Professional Engineer Email Address: dbuff@golder.com
	Professional Engineer Statement:
٥.	I, the undersigned, hereby certify, except as particularly noted herein*, that:
	(1) To the best of my knowledge, there is reasonable assurance that the air pollutant emissions unit(s) and the air pollution control equipment described in this application for air permit, when properly operated and maintained, will comply with all applicable standards for control of air pollutant emissions found in the Florida Statutes and rules of the Department of Environmental Protection; and
	(2) To the best of my knowledge, any emission estimates reported or relied on in this application are true, accurate, and complete and are either based upon reasonable techniques available for calculating emissions or, for emission estimates of hazardous air pollutants not regulated for an emissions unit addressed in this application, based solely upon the materials, information and calculations submitted with this application.
	(3) If the purpose of this application is to obtain a Title V air operation permit (check here \square , if so), I further certify that each emissions unit described in this application for air permit, when properly operated and maintained, will comply with the applicable requirements identified in this application to which the unit is subject, except those emissions units for which a compliance plan and schedule is submitted with this application.
	(4) If the purpose of this application is to obtain an air construction permit (check here \square , if so) or concurrently process and obtain an air construction permit and a Title V air operation permit revision or renewal for one or more proposed new or modified emissions units (check here \square , if so), I further certify that the engineering features of each such emissions unit described in this application have been designed or examined by me or individuals under my direct supervision and found to be in conformity with sound engineering principles applicable to the control of emissions of the air pollutants characterized in this application.
Maril	(5) If the purpose of this application is to obtain an initial air operation permit or operation permit revision or renewal for one or more newly constructed or modified emissions units (check here a fiss), I further certify that, with the exception of any changes detailed as part of this application, each such emissions unit has been constructed or modified in substantial accordance with the information given in the corresponding application for air construction permit and with all provisions confusined in such permit.
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3	* Attach any exception to certification statement.
3/2	្ទឹ*Board of Professional Engineers Certificate of Authorization #00001670
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DEP Form No. 62-210.900(1) - Form Effective: 06/16/03

APPLICATION INFORMATION

Application Responsible Official Certification

Complete if applying for an initial/revised/renewal Title V permit or concurrent processing of an air construction permit and a revised/renewal Title V permit. If there are multiple responsible officials, the "application responsible official" need not be the "primary responsible official."

Ricardo A. Lima, Vice President and General Manager							
Application Responsible Official Qualification (Check one or more of the following options, as applicable):							
For a corporation, the president, secretary, treasurer, or vice-president of the corporation in charge of a principal business function, or any other person who performs similar policy or decision-making functions for the corporation, or a duly authorized representative of such person if the representative is responsible for the overall operation of one or more manufacturing, production, or operating facilities applying for or subject to a permit under Chapter 62-213, F.A.C.							
For a partnership or sole proprietorship, a general partner or the proprietor, respectively.							
For a municipality, county, state, federal, or other public agency, either a principal executive officer or ranking elected official.							
The designated representative at an Acid Rain source.							
Application Responsible Official Mailing Address Organization/Firm: Okeelanta Corporation							
Street Address: 21250 U.S. Highway 27 South							
City: South Bay State: FL Zip Code: 33493							
Application Responsible Official Telephone Numbers							
Telephone: (561) 993-1600 ext. Fax: (561) 992-7326							
Application Responsible Official Email Address:							
Application Responsible Official Certification:							
I, the undersigned, am a responsible official of the Title V source addressed in this air permit application. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements made in this application are true, accurate and complete and that, to the best of my knowledge, any estimates of emissions reported in this application are based upon reasonable techniques for calculating emissions. The air pollutant emissions units and air pollution control equipment described in this application will be operated and maintained so as to comply with all applicable standards for control of air pollutant emissions found in the statutes of the State of Florida and rules of the Department of Environmental Protection and revisions thereof and all other applicable requirements identified in this application to which the Title V source is subject. I understand that a permit, if granted by the department, cannot be transferred without authorization from the department, and I will promptly notify the department upon sale or legal transfer of the facility or any permitted emissions unit. Finally, I certify that the facility and each emissions unit are in compliance with all applicable requirements to which they are subject, except as identified in compliance plan(s) submitted with this application. Signature Date							

DEP Form No. 62-210.900(1) – Form Effective: 06/16/03

VISIBLE EMISSIONS OBSERVATION FORMS

South Florida Environmental Services

VISIBLE EMISSIONS TEST REPORT

PREPARED FOR:

OKEELANTA CORPORATION 21250 US HIGHWAY 27 SOUTH BAY, FLORIDA

CONCERNING:

Visible Emissions Test Program
Eleven Emissions Units
Okeelanta Corporation
South Bay, Florida
September 21-22, 2003

PREPARED BY:

South Florida Environmental Services, LLC 6861 Vista Parkway North West Palm beach, Florida 33411

I hereby certify that the information contained in this report is true and accurate to the best of my knowledge.

Francis K. Morlu

Manager, Technical Operations

Date

COMPENDIUM:

At the request of Okeelanta Corporation and in compliance with the Florida Statues [62-297.310(4)(a)2, F.A.C.], as stipulated in their permit (No. 0990005-003-AV), South Florida Environmental Services performed Compliance Testing for Visible Emissions at Okeelanta Corporation on September 21 & 22, 2004. Testing was conducted on eleven of the twelve Emissions Units that are not subject to a multiple-valued opacity standard (potential PM Emissions < 100 tons per year). Emissions Unit # 028 was tested on 6/11/04.

During the compliance test, all units were observed to be operating at normal condition. The test on each unit was conducted for a thirty-minute period. All testing and data reduction were conducted in accordance with EPA Method 9 as found in 40 CFR 60 Appendix A, as amended.

Francis K Morlu and John Jallah of South Florida Environmental Services were the Certified Visible Emissions Evaluators at the time of testing. Mr. Mathew Capone, Director of Environmental Programs, was responsible for coordinating the plant operation.

The results (summarized in Table 1), show that all the Emissions Units are operating in compliance with Florida Statues and as required by regulatory conditions stipulated in their permit (No. 0990005-003-AV).

Table 1: Summary of Results

	Highest Six Minute Average Opacity (%)		
EU 018*		-	-
EU 019	0.0 %	0.0	5
EU 020	0.0%	0.0	5
EU 021	0.0%	0.0	5
EU 022	0.0%	0.0	5
EU 023*	•	-	-
EU 024*	•	-	-
EU 025	0.0%	0.0	5
EU 026	0.0%	0.0	5
EU 027	0.0%	0,0	5
EU 0287	•	· _ ,	-
EU 034	0.0%	0.0	5
EU 035	0.0%	0.0	5.
EUO46	0.0%	0.0	5
EU 047	0.0%	0.0	. 5



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ATTACHMENT B

DETAILED DESCRIPTION OF CONTROL EQUIPMENT

TABLE B-1
CONTROL EQUIPMENT PARAMETERS AND PARTICULATE REMOVAL EFFICIENCIES FOR SUGAR DUST WET COLLECTION SYSTEMS AT OKEELANTA SUGAR REFINERY

	Rotary Dryer	Conveying	Cooler No. 1	Cooler No. 2
Name	Wet Rotoclone	Wet Rotoclone	Wet Rotoclone	Wet Rotoclone
	No. 1	No. 2	No. 3	No. 4
ID Designation	. 021	022	023	024
Manufacturer	American Air	American Air	American Air	American Air
	Filter (AAF)	Filter (AAF)	Filter (AAF)	Filter (AAF)
Type/Design	Wet Rotoclone	Wet Rotoclone	Wet Rotoclone	Wet Rotoclone
	Type W, Size 27			
Outlet Gas Temp (°F)	100	100	100	100
Outlet Gas Flow Rate (acfm)	15,000	15,000	15,000	15,000
Water Injection Rate	,	,		
(gal/min) (minimum) ^a	2.2	2.2	2 to 9	2 to 9
Pressure Drop Across Device			,	
(inches H ₂ O) (min) ^a	6.8	6.8	2 to 9	2 to 9
Total PM Control Efficiency (%) ^b	99.9	99.9	99.9	99.9
Total PM ₁₀ Control Efficiency (%) ^b	99.0	99.0	99.0	99.0

Sample calculations:

Control efficiency (%) = [(inlet loading rate - outlet loading rate) / inlet loading rate] X = 100

Footnotes:

^a Based on 2002 stack testing for Rotoclones No. 1 and 2, and manufacturer's data for Rotoclones No. 3 and 4.

^b Control efficiency is manufacturer's efficieny rating.

TABLE B-2

CONTROL EQUIPMENT PARAMETERS AND PARTICULATE REMOVAL EFFICIENCY DERIVATION FOR FLUIDIZED BED DRYER/COOLER PULSE JET BAGHOUSE (EU 025) AT OKEELANTA SUGAR REFINERY

Manufacturer			BETH GmbH, 23556 Lobeck
Туре			BETHPULS 6.60 x 7.5.10
Outlet Gas Temp (°F)			115
Outlet Gas Flow Rate (acfm)	· -	<u></u>	70,620
Exhaust Gas Moisture Content (%)			0.7
Cleaning Method			Pulse Jet Compressed Air
Compressed Air Consumption (cfm)			51.8
Number of Bags			. 420
Total Filter Media Surface Area (sq. ft)	·		9,041
Air to Cloth Ratio (cfm per sq ft.)			7.81
Outlet Loading (grains/dscf)			0.00348
,	Inlet ^b	Control ^c	Outlet
	Loading	Efficiency	Loading
Pollutant	(lb/hr)	(%)	(lb/hr)
Particulate Matter	960	99.80	1.92

Note: All parameters are based on manufacturers design information.

Footnotes:

^a Calculated based on expected outlet loading rate (lb/hr) and outlet gas flow rate (scfm) at operational conditions.

Sample calculations:

Outlet loading rate = inlet loading rate X [1-(control efficiency/100)].

b Inlet loading to the filter specified by the fluidized bed dryer manufacturer while operating at Okeelanta's estimated maximum refined sugar production (includes a 20% design safety factor).

^c Control efficiency based on baghouse manufacturers design information for dust content in raw gas (10g/m³ at standard conditions) and for dust content in clean gas (20 mg/m³ at standard conditions).

ATTACHMENT B-3

DETAILED DESCRIPTION OF CONTROL EQUIPMENT FOR COGENERATION BOILERS A, B, AND C

The cogeneration facility utilizes several emission control techniques to reduce emissions. A selective non-catalytic reduction (SNCR) system is used to reduce NO_x emissions. Further, the cogeneration boilers minimize CO and VOC through proper furnace design and good combustion practices, including control of combustion air and combustion temperature, distribution of fuel on the combustion grate, and control over the furnace loads and transient conditions. Particulate emissions are controlled by an electrostatic precipitator (ESP). Multiple cyclones were installed during the 2000 calendar year to improve control of particulate emissions. Mercury emissions are controlled through a carbon injection system and the ESP system.

Electrostatic Precipitator

The EPSs for the New Hope Power Partnership (NHPP) facility are manufactured by Flakt, Inc. Design specifications for the ESP (one per boiler) are provided below:

Chambers = 1

Collecting Plate = 12.30 ft L x 39.37 ft H

Fields/Chamber = 3

Specific Collection Area = $200 \text{ ft}^2/1,000 \text{ acfm (minimum)}$

Gas Velocity = <4 ft/s

Pressure Drop = less than 2.8 inches H_2O

Operating Temperature = 350°F

Ash Handling = Trough hopper with screw conveyor

Particulate removal efficiency: >99.2%

NO_x Control System

The NO_x control system design employs a urea injection system manufactured by Nalco-Fueltech for NO_x control. The technology is a SNCR process, which reduces NO_x emissions through chemical reaction with urea. In the process, urea is injected into the flue gas stream and reacts with NO_x to form nitrogen and water vapor.

The NO_x control system includes the following major components:

- Carrier air compressors,
- Urea tank,
- Urea/air flow controls,
- Control panel,
- Injection manifolds and injectors, and
- Valves and instrumentation.

A single urea storage tank system is installed to supply urea to all three boilers. Urea for injection into the boilers is drawn from the tank. Two injection zones are used to provide injection at full and part load conditions. Each zone has six injectors. Zone switching valves will direct the urea/carrier mixture to the appropriate injection zone.

Specifications for the urea injection system to meet the NO_x emission rate of 0.15 lb/MMBtu when firing biomass or No. 2 fuel oil are provided below (on a per boiler basis):

Urea injection rate - 65 gal/hr (max)

Ammonia Slip - Biomass, No. 2 fuel oil, natural gas - 25 ppm (max)

Mercury Control System

The mercury control system is supplied by ABB Environmental Systems and Chemco, Inc. A volumetric feeder with integral supply hopper meters activated carbon for injection at a point in the ductwork between the ESP and the ID fan. This promotes turbulent mixing and provides adequate residence time. A blower system transports the carbon to the injection point. The ESP will effectively capture the activated carbon particles along with the boiler fly ash (which also contains some carbon). The system is designed to inject up to 13 lb/hr of carbon into the flue gases of each boiler.

Dust Control System

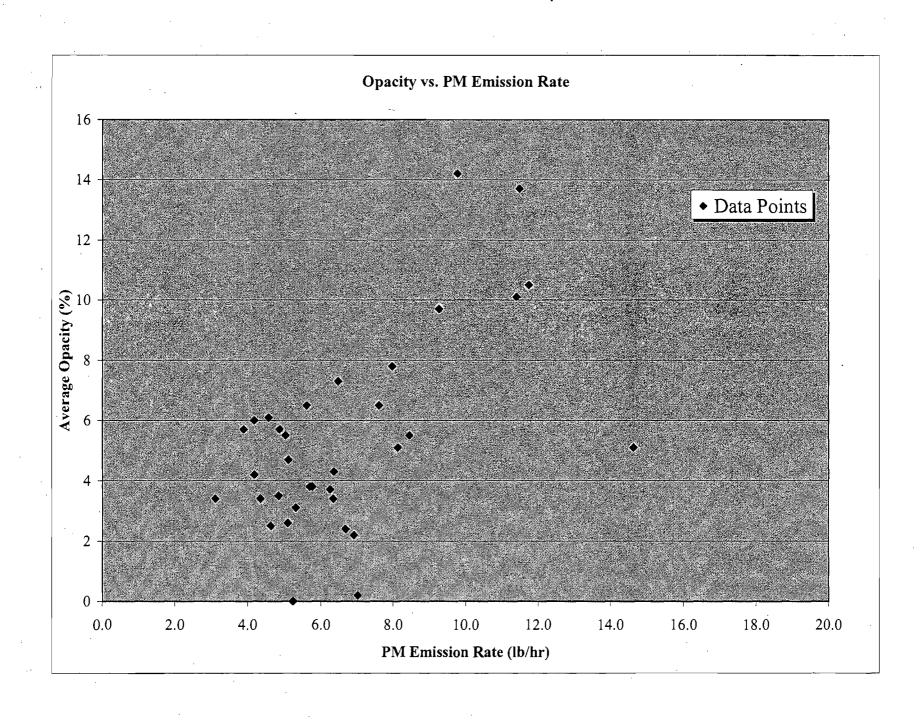
The cyclone dust collectors are supplied by Barron Industries, Model 460 Tube Base III 9K15-2023 AU. These are mechanical cyclone dust collectors which remove larger size particulate matter prior to the ESP. There are 460 cyclone tubes in all.

ATTACHMENT C

OPACITY DATA

Table C-1. NHPP Cogeneration Facility Stack Opacity Test Data Summary

	_			Average Opacity	Average PM	
Boiler	Run	Period Start	Period End	(%)	lb/MMBtu	lb/hr
A	Run 1	2/24/2005 1:31:00 PM	2/24/2005 2:38:00 PM	9.7	0.0138	9.27
Λ.	Run 2	2/24/2005 3:08:00 PM	2/24/2005 4:11:00 PM	10.1	0.0138	11.40
	Run 3	2/24/2005 4:47:00 PM	2/24/2005 4:11:00 PM 2/24/2005 5:45:00 PM	10.5	0.0177	11.75
	Run 1	2/16/2004 9:15:00 AM	2/16/2004 10:21:00 AM	. 3.4	0.0172	3.11
	Run 2	2/16/2004 11:01:00 AM	2/16/2004 10:21:00 AM 2/16/2004 12:05:00 PM	2.6	0.0032	5.11
	Run 3	2/16/2004 11:01:00 AM 2/16/2004 12:47:00 PM	2/16/2004 1:49:00 PM	2.5	0.0030	4.63
	Run 1	1/22/2003 9:43:00 AM	1/22/2003 11:42:00 AM	3.4	0.0072	6.34
	Run 2	1/22/2003	1/22/2003 11:42:00 AM 1/22/2003 1:20:00 PM	2.4	0.0083	6.68
	Run 3	1/22/2003 12:17:00 PM	1/22/2003 1:20:00 PM	2.2	0.0090	6.91
	Run 1	2/13/2002 10:16:00 AM	2/13/2002 11:19:00 AM	5.5	0.0093	8.45
	Run 2	2/13/2002 10:10:00 AM 2/13/2002 12:09:00 PM	2/13/2002 1:13:00 PM	4.7	0.0110	5.11
	Run 3	2/13/2002 1:44:00 PM	2/13/2002 1:13:00 PM	4.2	0.0070	4.18
	Kun 5	2/13/2002 1.44.00 1 W	2/13/2002 2.48.00 FW	4.2	0.00,50	4.10
3	Run 1	2/23/2005 1:55:00 PM	2/23/2005 3:01:00 PM	14.2	0.0143	9.78
	Run 2	2/23/2005 3:46:00 PM	2/23/2005 4:49:00 PM	13.7	0.0174	11.49
	Run 3	2/24/2005 9:23:00 AM	2/24/2005 10:27:00 AM	7.8	0.0117	7.98
	Run 1	2/13/2004 8:52:00 AM	2/13/2004 9:54:00 AM	7.3	0.0101	6.48
	Run 2	2/13/2004 12:40:00 PM	2/13/2004 1:44:00 PM	5.5	0.0077	5.03
	Run 3	2/13/2004 2:27:00 PM	2/13/2004 3:32:00 PM	6.5	0.0115	7.62
	Run 1	1/23/2003 10:58:00 AM	1/23/2003 12:01:00 PM	3.7	0.0088	6.26
	Run 2	1/23/2003 12:31:00 PM	1/23/2003 1:34:00 PM	3.8	0.0082	5.76
	Run 3	1/23/2003 2:01:00 PM	1/23/2003 3:04:00 PM	3.5	0.0067	4.84
	Run 1	2/14/2002 9:35:00 AM	2/14/2002 10:39:00 AM	5.1	0.0110	8.12
	Run 2	2/14/2002 11:10:00 AM	2/14/2002 12:15:00 PM	4.3	0.0090	6.36
	Run 3	2/14/2002 12:49:00 PM	2/14/2002 1:54:00 PM	3.8	0.0080	5.70
	Run 1	2/22/2005 2:15:00 PM	2/22/2005 3:19:00 PM	6.5	0.0132	5.62
	Run 3	2/23/2005 8:53:00 AM	2/23/2005 9:56:00 AM	6	0.0060	4.18
	Run 1	2/11/2004 9:50:00 AM	2/11/2004 10:54:00 AM	6.1	0.0072	4.57
	Run 2	2/11/2004 11:36:00 AM	2/11/2004 12:42:00 PM	5.7	0.0080	4.87
	Run 3	2/11/2004 1:20:00 PM	2/11/2004 2:25:00 PM	5.7	0.0062	3.90
	Run 1	1/21/2003 12:16:00 PM	1/21/2003 1:21:00 PM	0	0.0074	5.23
	Run 2	1/21/2003 2:07:00 PM	1/21/2003 3:10:00 PM	0	0.0072	5.24
	Run 3	1/21/2003 4:13:00 PM	1/21/2003 5:24:00 PM	0.2	0.0096	7.01
	Run 1	2/12/2002 10:14:00 AM	2/12/2002 11:19:00 AM	5.1	0.0190	14.63
	Run 2	2/12/2002 12:35:00 PM	2/12/2002 1:39:00 PM	3.1	0.0070	5.31
	Run 3	2/12/2002 2:11:00 PM	2/12/2002 3:15:00 PM	3.4	0.0060	4.35



Company: Okeelanta CoGen Period Start:

02/24/2005 08:53

Plant:

2/24/2005

2/24/2005

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14:12

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South Bay, FL

Period End: 02/24/2005 Validation Type:

09:56

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1/1 min

Averaging Period:

1 min

Type: Block Avg

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	(Opacity 1			Opacity 1
Period Start		%	Period Start		%
2/24/2005	13:31	7	2/24/2005	14:13	9.8
2/24/2005	13:32	6.8	2/24/2005	14:14	9.8
2/24/2005	13:33	6.7	2/24/2005	14:15	13.4
2/24/2005	13:34	6.8	2/24/2005	14:16	10.2
2/24/2005	13:35	7	2/24/2005	14:17	12.6
2/24/2005	13:36	7.3	2/24/2005	14:18	9.7
2/24/2005	13:37	12.9	2/24/2005	14:19	10
2/24/2005	13:38	9.6	2/24/2005	14:20	8.6
2/24/2005	13:39	7.2	2/24/2005	14:21	9.7
2/24/2005	13:40	7.1	2/24/2005	14:22	9.4
2/24/2005	13:41	7.8	2/24/2005	14:23	16.7
2/24/2005	13:42	7.7	2/24/2005	14:24	13.8
2/24/2005	13:43	6.8	2/24/2005	14:25	20.3
2/24/2005	13:44	7.1	2/24/2005	14:26	10.3
2/24/2005	13:45	7.2	2/24/2005	14:27	9.9
2/24/2005	13:46	7.3	2/24/2005	14:28	9.2
2/24/2005	13:47	6.8	2/24/2005	14:29	10.3
2/24/2005	13:48	6.9	2/24/2005	14:30	15.3
2/24/2005	13:49	6.5	2/24/2005	14:31	11.3
2/24/2005	13:50	7.4	2/24/2005	14:32	9.2
2/24/2005	13:51	8.6	2/24/2005	14:33	9.3
2/24/2005	13:52	9.9	2/24/2005	14:34	8.9
2/24/2005	13:53	7.4	2/24/2005	14:35	8.0
2/24/2005	13:54	6.8	2/24/2005	14:36	11.6
2/24/2005	13:55	6.8	2/24/2005	14:37	8.1
. 2/24/2005	13:56	8.3	2/24/2005	14:38	21.1
2/24/2005	13:57	7.3	Final Average*	•	9.7
2/24/2005	13:58	8.2	Maximum*		23.40
2/24/2005	13:59.	8.	Minimum*		6.50
2/24/2005	14:00	. 8			
2/24/2005	14:01	23.4	*Does not include I	nvalid Av	eraging Period
2/24/2005	14:02	10.3			0 0
2/24/2005	14:03	9.3			
2/24/2005	14:04	8.3			
2/24/2005	14:05	7.8			
2/24/2005	14:06	9.9			
2/24/2005	14:07	8.4			
2/24/2005	14:08	15.2			
2/24/2005	14:09	10.7			
2/24/2005	14:10	12.1			
0/04/0005	1 1 1 1	0.7			

Periods ("N/A")

Company: Okeelanta CoGen Period Start:

02/24/2005

15:08

Plant:

Stack 1

Period End:

02/24/2005

16:11

City/St: Source:

2/24/2005

15:49

13.7

South Bay, FL

Validation Type:

1/1 min

Averaging Period:

1 min

Type:

Block Avg

		verage			Average
	· O _l	pacity_1		O	pacity_1
eriod Start		%	Period Start		%
2/24/2005	15:08	6.8	2/24/2005	15:50	. 9.6
2/24/2005	15:09	7.1	2/24/2005	15:51	13
2/24/2005	15:10	8.2	2/24/2005	15:52	10.5
2/24/2005	15:11	8.7	2/24/2005	15:53	9.7
2/24/2005	15:12	8.4	2/24/2005	15:54	10.3
2/24/2005	15:13	7	2/24/2005	15:55	9.5
2/24/2005	15:14	7.1	2/24/2005	15:56	11.5
2/24/2005	15:15	7.2	2/24/2005	15:57	9.9
2/24/2005	15:16	7.4	2/24/2005	15:58	9.5
2/24/2005	15:17	7.5	2/24/2005	15:59	11.1
2/24/2005	15:18	7.2	2/24/2005	16:00	10.6
2/24/2005	15:19	8.2	2/24/2005	16:01	8.9
2/24/2005	15:20	8.3	2/24/2005	16:02	9.6
2/24/2005	15:21	7.5	2/24/2005	16:03	11.4
2/24/2005	15:22	7.3	2/24/2005	16:04	9.7
2/24/2005	15:23	10.3	2/24/2005	16:05	8.8
2/24/2005	15:24	10.2	2/24/2005	16:06	9.8
2/24/2005	15:25	9	2/24/2005	16:07	9.7
2/24/2005	15:26	8.8	2/24/2005	16:08	10.8
2/24/2005	15:27	8.1	2/24/2005	16:09	9.1
2/24/2005	15:28	10.7	2/24/2005	16:10	. 9
2/24/2005	15:29	9.3	2/24/2005	16:11	10
2/24/2005	15:30	9.1	Final Average*		10.1
2/24/2005	15:31	9.9	Maximum*		38.0
2/24/2005	15:32	9.3	Minimum*		6.8
2/24/2005	15:33	8.5	***************************************		0.0
2/24/2005	15:34	8.1	*Does not include l	nvalid Aver	aging Periods
2/24/2005	15:35	8.7	Boos not morade i		aging renous
2/24/2005	15:36	11.1			
2/24/2005	15:37	9.4			
2/24/2005	15:38	38			
2/24/2005	15:39	11.3			
2/24/2005	15:40	10.2			
2/24/2005	15:41	13.3			
2/24/2005	15:42	14.3			
2/24/2005	15:43	14.3	1		
2/24/2005	15:44	11.3			
2/24/2005	15:45	11.5			
2/24/2005	15:46	11.3		•	
2/24/2005	15:47	9.3			
2/24/2005	15:48	9.3 9.8		•	
212412003	13.40	7.0			

Company: Okeelanta CoGen

Period Start:

02/24/2005 16:47

Plant:

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

2/24/2005

- 2/24/2005

17:08

17:09

17:10

17:11

17:12

17:13

17:14

17:15

17:16

17:17

17:18

17:19

17:20

17:21

17:22

17:23

17:24

17:25

17:26

17:27

17:28

Plant:

Period End:

17:45

City/St:

South Bay, FL

Validation Type:

02/24/2005 1/1 min

Source:

Stack 1

Averaging Period:

1 min

Type: Block Avg

		Average Opacity_1			Average Opacity_1
Period Start		%	Period Start		%
2/24/2005	16:47	7.5	2/24/2005	17:29	13.1
2/24/2005	16:48	8.4	2/24/2005	17:30	14.3
2/24/2005	16:49	8.3	2/24/2005	17:31	12.1
2/24/2005	16:50	8.1	2/24/2005	17:32	12.8
2/24/2005	16:51	11.6	2/24/2005	17:33	11.9
2/24/2005	16:52	10.7	2/24/2005	17:34	11.3
2/24/2005	16:53	8.1	2/24/2005	17:35	11
2/24/2005	16:54	7.3	2/24/2005	17:36	13.9
2/24/2005	16:55	8.3	2/24/2005	17:37	12.5
2/24/2005	16:56	8.6	2/24/2005	17:38	12.8
2/24/2005	16:57	9	2/24/2005	17:39	13.2
2/24/2005	16:58	9	2/24/2005	17:40	12.1
2/24/2005	16:59	8.9	2/24/2005	17:41	12.1
2/24/2005	17:00	11.7	2/24/2005	17:42	12
2/24/2005	17:01	9.1	2/24/2005	17:43	12.2
2/24/2005	17:02	8.8	2/24/2005	17:44	17.9
2/24/2005	17:03	8.1	2/24/2005	17:45	12.3
2/24/2005	17:04	8.7	Final Average*		10.5
2/24/2005	17:05	7.6	Maximum*		17.9
2/24/2005	17:06	8.5	Minimum*		7.3
2/24/2005	17:07	7.9			

7.5

7.6

8.2

7.8

9.3

9.5

10

12.2

10.7

10.8

9.8

10.1

9.7

11

11.2

11.1

12.8

13.9

12.2

12.3

12

^{*}Does not include Invalid Averaging Periods ("N/A")

Company: Okeelanta CoGen

Period Start: 02/23/2005 13:55

Plant:

Period End:

02/23/2005 15:01

City/St: South Bay, FL

Validation Type:

1/1 min

Source: Stack 2

Averaging Period: 1 min

	A	Average		,	Average	
	C	pacity 1		. (Opacity 1	
Period Start		%	Period Start		%	
2/23/2005	13:55	8.1	2/23/2005	14:37	22.1	
2/23/2005	13:56	7.9	2/23/2005	14:38	32.2	
2/23/2005	13:57	7.4	2/23/2005	14:39	23.2	
2/23/2005	13:58	7.5	2/23/2005	14:40	12.7	
2/23/2005	13:59	7.8	2/23/2005	14:41	15.1	
2/23/2005	14:00	11.6	2/23/2005	14:42	12.2	
2/23/2005	14:01	13.4	2/23/2005	14:43	10.6	
2/23/2005	14:02	13.9	2/23/2005	14:44	11.7	
2/23/2005	14:03	10	2/23/2005	14:45	9.5	
2/23/2005	14:04	11.5	2/23/2005	14:46	9.9	
2/23/2005	14:05	11.6	2/23/2005	14:47	13.2	
2/23/2005	14:06	10.7	2/23/2005	14:48	11.3	
2/23/2005	14:07	14.9	2/23/2005	14:49	10.2	
2/23/2005	14:08	11.7	2/23/2005	14:50	9.8	
2/23/2005	14:09	11.8	2/23/2005	14:51	14.6	
2/23/2005	14:10	14.7	2/23/2005	14:52	9.9	
2/23/2005	14:11	. 15	2/23/2005	14:53	10.5	
2/23/2005	14:12	11.3	2/23/2005	14:54	10.3	
2/23/2005	14:13	13.4	2/23/2005	14:55	9.1	
2/23/2005	14:14	11.7	2/23/2005	14:56	8.2	
2/23/2005	14:15	12.3	2/23/2005	14:57	7.5	
2/23/2005	14:16	17.9	2/23/2005	14:58	8.5	
2/23/2005	14:17	17.9	2/23/2005	14:59	10.0	
2/23/2005	14:18	12.2	2/23/2005	15:00	10.9	
2/23/2005	14:19	16.9	2/23/2005	15:01	8.7	
2/23/2005	14:20	13.9	Final Average*		14.2	
2/23/2005	14:21	13	Maximum*		32.20	
2/23/2005	14:22	16.4	Minimum*		7.40	
2/23/2005	14:23	17.3				
2/23/2005	14:24	13.7	*Does not include I	nvalid Ave	raging Periods ('N/A")
2/23/2005	14:25	14.8				,
2/23/2005	14:26	22.9				•
2/23/2005	14:27	21.9	•			
2/23/2005	14:28	23.4				
2/23/2005	14:29	23.9				
2/23/2005	14:30	18.2				
2/23/2005	14:31	24.2				
2/23/2005	14:32	28.9				
2/23/2005	14:33	19.7	· .			
2/23/2005	14:34	19.4		,		
2/23/2005	14:35	27.2		,		
2/23/2005	14:36	19.6	•			

Company: Okeelanta CoGen

Period Start: 02/23/2005 15:46

Plant:

2/23/2005

2/23/2005

2/23/2005

2/23/2005

2/23/2005

2/23/2005

2/23/2005

2/23/2005

2/23/2005

16:19

16:20

16:21

16:22

16:23

16:24

16:25

16:26

16:27

15.2

15.9

13.5

11.2

11.1

17.2

14.2

11.9

18.3

Period End:

02/23/2005 16:49

City/St: South Bay, FL

Validation Type:

nin

Source: Stack 2

Averaging Period:

1/1 min 1 min

Type:

Block Avg

		Average pacity 1			Average
Period Start	Opacity_1 %		Period Start	Opacity_1 %	
2/23/2005	15:46	10.1	2/23/2005	16:28	16.3
2/23/2005	15:47	8.6	2/23/2005	16:29	11.8
2/23/2005	15:48	8.4	2/23/2005	16:30	11.5
2/23/2005	15:49	9.6	2/23/2005	16:31	13.5
2/23/2005	15:50	13.9	2/23/2005	16:32	16.6
2/23/2005	. 15:51	16.1	2/23/2005	16:33	11.9
2/23/2005	15:52	11.3	2/23/2005	16:34	12.4
2/23/2005	15:53	8.3	2/23/2005	16:35	10.8
2/23/2005	15:54	8.7	2/23/2005	16:36	12
2/23/2005	15:55	10.6	2/23/2005	16:37	19.9
2/23/2005	15:56	11.9	2/23/2005	16:38	19.4
2/23/2005	15:57	9.4	2/23/2005	16:39	15.1
2/23/2005	15:58	9.4	2/23/2005	16:40	13.4
2/23/2005	15:59	12	2/23/2005	16:41	10.7
2/23/2005	16:00	11.3	2/23/2005	16:42	14.1
2/23/2005	16:01	10.7	2/23/2005	16:43	14.7
2/23/2005	16:02	· 14	2/23/2005	16:44	13.5
2/23/2005	16:03	10.5	2/23/2005	16:45	18.9
2/23/2005	16:04	11.4	2/23/2005	16:46	17.6
2/23/2005	16:05	11.6	2/23/2005	16:47	23.3
2/23/2005	16:06	11	2/23/2005	16:48	17.8
2/23/2005	16:07	15.4	2/23/2005	16:49	19
2/23/2005	16:08	27.3	Final Average*		13.7
2/23/2005	16:09	12.1	Maximum*		27.30
2/23/2005	16:10	12.2	Minimum*		8.30
2/23/2005	16:11	21.5			
2/23/2005	16:12	18.8	*Does not include l	nvalid Avera	aging Periods ("N/A
2/23/2005	16:13	13.8			
2/23/2005	16:14	11.8			
2/23/2005	16:15	12.9			
2/23/2005	16:16	12.1			
2/23/2005	16:17	11.8			
2/23/2005	16:18	13.5			
0/00/0005	16 10	4 - 4			

Company: Okeelanta CoGen

Period Start: 02/24/2005 09:23 Period End: 02/24/2005 10:27

Plant:

2/24/2005

10:04

7.9

Period Star

City/St: South Bay, FL

Period End: 02/24/2005 Validation Type: 1/1 min

Source: Stack 2

Averaging Period: 1 min

	A	verage		A	verage	
•	O	pacity 1		O	pacity 1	
Period Start	_	%	Period Start	•	%	
2/24/2005	9:23	7.4	2/24/2005	10:05	7.9	
2/24/2005	9:24	10.5	2/24/2005	10:06	7.4	
2/24/2005	9:25	8.2	2/24/2005	10:07	7.3	
2/24/2005	9:26	7.8	2/24/2005	10:08	. 7.1	
2/24/2005	9:27	7.3	2/24/2005	10:09	7.1	
2/24/2005	9:28	7.6	2/24/2005	10:10	7.4	
2/24/2005	9:29	8.1	2/24/2005	10:11	7.2	
2/24/2005	9:30	7.8	2/24/2005	10:12	7.6	
2/24/2005	9:31	7.5	2/24/2005	10:13	7.3	
2/24/2005	9:32	7.3	2/24/2005	10:14	7.7	
2/24/2005	9:33	6.9	2/24/2005	10:15	7.1	
2/24/2005	9:34	6.8	2/24/2005	10:16	7.2	
2/24/2005	9:35	7	2/24/2005	10:17	7.2	
2/24/2005	9:36	7	2/24/2005	10:18	8.3	
2/24/2005	9:37	6.9	2/24/2005	10:19	7.2	
2/24/2005	9:38	6.6	2/24/2005	10:20	6.9	
2/24/2005	9:39	6.5	2/24/2005	10:21	7.1	
2/24/2005	9:40	6.7	2/24/2005	10:22	7.1	
2/24/2005	9:41	6.6	2/24/2005	10:23	7.5	•
2/24/2005	9:42	6.9	2/24/2005	10:24	7.3	
2/24/2005	9:43	6.9	2/24/2005	10:25	8.2	
2/24/2005	9:44	6.8	2/24/2005	10:26	22.2	
2/24/2005	9:45	6.8	2/24/2005	10:27	18.4	
2/24/2005	9:46	9	Final Average*		7.8	
2/24/2005	9:47	7.3	Maximum*		22.20	
2/24/2005	9:48	7.1	Minimum*	•	6.50	
2/24/2005	9:49	7.3				
2/24/2005	9:50	7.1	*Does not include I	nvalid Avera	ging Periods ("N	√A")
2/24/2005	9:51	7.5	•			
2/24/2005	9:52	7.6				
2/24/2005	9:53	7.8				
2/24/2005	9:54	7		•		
2/24/2005	9:55	. 8				
2/24/2005	9:56	6.9				•
2/24/2005	9:57	8.2				
2/24/2005	9:58	7.4				
2/24/2005	9:59	7.1				
2/24/2005	10:00	6.9				
2/24/2005	10:01	7.1				
2/24/2005	10:02	7.5				
2/24/2005	10:03	8.2			•	
0 10 1 10 0 0 5	4004					

Company: Okeelanta CoGen Period Start: 02/22/2005

14:15

Plant: City/St:

South Bay, FL

02/22/2005 15:19

Validation Type:

1/1 min

Source: Stack 3 Averaging Period: 1 min

Period End:

D 1.10		erage acity_1	n		verage pacity_1
Period Start		%	Period Start		%
2/22/2005	14:15	5.5	2/22/2005	14:57	5.4
2/22/2005	14:16	5.8	2/22/2005	14:58	5.4
2/22/2005	14:17	5.5	2/22/2005	14:59	5.3
2/22/2005	14:18	5.7	2/22/2005	15:00	5.3
2/22/2005	14:19	7.9	2/22/2005	15:01	5.3
2/22/2005	14:20	15	2/22/2005	15:02	6.2
2/22/2005	14:21	9.1	2/22/2005	15:03	44.9
2/22/2005	14:22	5.8	2/22/2005	15:04	9.2
2/22/2005	14:23	5.5	2/22/2005	15:05	5.4
2/22/2005	14:24	7.5	2/22/2005	15:06	5.4
2/22/2005	14:25	6.1	2/22/2005	15:07	5.4
2/22/2005	14:26	5.6	2/22/2005	15:08	5.5
2/22/2005	14:27	5.6	2/22/2005	15:09	5.3
2/22/2005	14:28	5.8	2/22/2005	15:10	5.3
2/22/2005	14:29	6.4	2/22/2005	15:11	5.3
2/22/2005	14:30	5.7	2/22/2005	15:12	5.3
2/22/2005	14:31	5.6	2/22/2005	15:13	5.2
2/22/2005	14:32	6.5	2/22/2005	15:14	5.3
2/22/2005	14:33	5.9	2/22/2005	15:15	5.2
2/22/2005	14:34	5.8	2/22/2005	15:16	5.4
2/22/2005	14:35	5.6	2/22/2005	15:17	5.5
2/22/2005	14:36	5.6	2/22/2005	15:18	5.5
2/22/2005	14:37	5.5	2/22/2005	15:19	5.4
2/22/2005	14:38	5.5	Final Average*		6.5
2/22/2005	14:39	5.5	Maximum*		44.9
2/22/2005	14:40	5.5	Minimum*		5.2
2/22/2005	14:41	5.3	1174		3.2
2/22/2005	14:42	5.8	*Does not include l	nvalid Avera	ring Periode ("N
2/22/2005	14:43	7	Does not metude i	arana Avela	sing i crious (I
2/22/2005	14:44	5.5			
2/22/2005	14:45	5.8			
2/22/2005	14:46	5.8 6.1			
2/22/2005	14:47	5.7			
2/22/2005	14:48	5.5			
2/22/2005	14:49	5.7			
2/22/2005	14:50	6.3			
2/22/2005	14:51	5.5	•		
2/22/2005	14.52	5.5 5.5			
2/22/2005	14:53	5.5 5.5			
2/22/2005	14:53	5.7			
2/22/2005	14:55	5.5			
2/22/2005	14:56	5.4			

Company: Okeelanta CoGen Period Start:

02/23/2005 08:53

Plant:

Period End:

02/23/2005 09:56

City/St: South Bay, FL Source: Stack 3

Validation Type: Averaging Period: 1/1 min

1 min

		verage pacity_1			verage pacity_1
Period Start		%	Period Start	•	%
2/23/2005	8:53	6	2/23/2005	9:35	6.1
2/23/2005	8:54	5.9	2/23/2005	9:36	6
2/23/2005	8:55	5.8	2/23/2005	9:37	6.3
2/23/2005	8:56	5.9	2/23/2005	9:38	6
2/23/2005	8:57	5.9	2/23/2005	9:39	6.1
2/23/2005	8:58	5.7	2/23/2005	9:40	6
2/23/2005	8:59	5.8	2/23/2005	9:41	6.1
2/23/2005	9:00	5.8	2/23/2005	9:42	6.1
2/23/2005	9:01	5.9	2/23/2005	9:43	6.4
2/23/2005	9:02	5.8	2/23/2005	9:44	6.4
2/23/2005	9:03	5.8	2/23/2005	9:45	6.4
2/23/2005	9:04	5.9	2/23/2005	9:46	6.4
2/23/2005	9:05	6	2/23/2005	9:47	6.3
2/23/2005	9:06	5.8	2/23/2005	9:48	6.2
2/23/2005	9:07	6	2/23/2005	9:49	6.5
2/23/2005	9:08	5.9	2/23/2005	9:50	6.3
2/23/2005	9:09	6.2	2/23/2005	9:51	6.1
2/23/2005	9:10	5.8	2/23/2005	9:52	6.1
2/23/2005	9:11	5.9	2/23/2005	9:53	6
2/23/2005	9:12	5.9	2/23/2005	9:54	6
2/23/2005	9:13	6	2/23/2005	9:55	5.9
2/23/2005	9:14	6	2/23/2005	9:56	6.1
2/23/2005	9:15	5.8	Final Average*		6.0
2/23/2005	9:16	5.9	Maximum*		6.5
2/23/2005	9:17	5.9	Minimum*		5.7
2/23/2005	9:18	5.9			
2/23/2005	9:19	. 6			
2/23/2005	9:20	6.3	*Does not include In	nvalid Averag	ging Periods ("N/A")
2/23/2005	9:21	5.9		. 2	, ,
2/23/2005	9:22	6.1			
2/23/2005	9:23	6			
2/23/2005	9:24	6			
2/23/2005	9:25	6			
2/23/2005	9:26	6			
2/23/2005	9:27	6			
2/23/2005	9:28	6.3			
2/23/2005	9:29	6.1			
2/23/2005	9:30	6			
2/23/2005	9:31	6.1			
2/23/2005	9:32	6.4			
2/23/2005	9:33	6.1			
2/23/2005	9:34	6			

Company: Okeelanta CoGen Period Start: 02/16/2004

Plant:

Period End:

02/16/2004

09:15 10:21

City/St: South Bay, FL Validation Type:

1/1 min

Source:

Averaging Period:

1 min

Stack 1

Type:

Block Avg

	Av	erage
		acity_1
eriod Start		%
2/16/2004	9:15	2.4
2/16/2004	9:16	2.4
2/16/2004	9.17	2.5

Period Start	•	%
2/16/2004	9:15	2.4
2/16/2004	9:16	2.4
2/16/2004	9:17	2.5
2/16/2004	9:18	2.3
2/16/2004	9:19	2.4
2/16/2004	9:20	2.3
2/16/2004	9:21	2.4
2/16/2004	9:22	2.3
2/16/2004	9:23	2.4
2/16/2004	9:24	2.4
2/16/2004	9:25	2.7
2/16/2004	9:26	2.7
2/16/2004	9:27	2.4
2/16/2004	9:28	2.5
2/16/2004	9:29	2.5
2/16/2004	9:30	2.5
2/16/2004	9:31	2.5
2/16/2004	9:32	2.5
2/16/2004	9:33	2.5
2/16/2004	9:34	2.6
2/16/2004	9:35	2.5
2/16/2004	9:36	2.5
2/16/2004	9:37	2.5
2/16/2004	9:38	2.5
2/16/2004	9:39	2.5
2/16/2004	9:40	2.5
2/16/2004	9:41	2.5
2/16/2004	9:42	2.6
2/16/2004	9:43	2.6
2/16/2004	9:44	2.7
2/16/2004	9:45	2.7

2/16/2004	9:43	2.6
2/16/2004	9:44	2.7
2/16/2004	9:45	2.7
2/16/2004	9:46	2.6
2/16/2004	9:47	3.1
2/16/2004	9:48	2.7
2/16/2004	9:49	2.8
2/16/2004	9:50	2.6
2/16/2004	9:51	. 2.7
2/16/2004	9:52	2.8
2/16/2004	9:53	3.2
2/16/2004	9:54	2.9

9:55

9:56

2.8

2.8

2/16/2004

2/16/2004

		Average
		Opacity_1
Period Start		%
2/16/2004	9:57	2.7
2/16/2004	9:58	3
2/16/2004	9:59	3.3
2/16/2004	10:00	3.2
2/16/2004	10:01	2.8
2/16/2004	10:02	2.7
2/16/2004	10:03	2.7
2/16/2004	10:04	2.9
2/16/2004	10:05	2.8
2/16/2004	10:06	2.8
2/16/2004	10:07	2.9
2/16/2004	10:08	3.2
2/16/2004	10:09	3.3
2/16/2004	10:10	2.8
2/16/2004	10:11	2.7
2/16/2004	10:12	2.8
2/16/2004	10:13	4.7
2/16/2004	10:14	5
2/16/2004	10:15	3.7
2/16/2004	10:16	34.1
2/16/2004	10:17	5.1
2/16/2004	10:18	6.6
2/16/2004	10:19	4
2/16/2004	10:20	3.6
2/16/2004	10:21	3.3
Final Average*		3.4
Maximum*		34.1

^{*}Does not include Invalid Averaging Periods ("N/A")

2.3

Minimum*

Company: Okeelanta CoGen Period Start: 02/16/2004 11:01 Plant: Period End: 02/16/2004 12:05

City/St: South Bay, FL Validation Type: 1/1 min Source: Stack 1 Averaging Period: 1 min

> Type: Block Avg

		Average Opacity_1			Average Opacity_1
Period Start		%	Period Start		%
2/16/2004	11:01	2.3	2/16/2004	11:43	2.7
2/16/2004	11:02	2.4	2/16/2004	11:44	2.5
2/16/2004	11:03	2.5	2/16/2004	11:45	3.1
2/16/2004	11:04	2.4	2/16/2004	11:46	2.5
2/16/2004	11:05	2.3	2/16/2004	11:47	2.6
2/16/2004	11:06	2.4	2/16/2004	11:48	2.9
2/16/2004	11:07	2.3	2/16/2004	11:49	2.9
2/16/2004	11:08	2.3	2/16/2004	11:50	2.7
2/16/2004	11:09	2.4	2/16/2004	11:51	2.8
2/16/2004	11:10	2.3	2/16/2004	11:52	2.6
2/16/2004	11:11	2.5	2/16/2004	11:53	3.4
2/16/2004	11:12	2.5	2/16/2004	11:54	3.2
2/16/2004	11:13	3	2/16/2004	11:55	3
2/16/2004	11:14	2.9	2/16/2004	11:56	3 3 3
2/16/2004	11:15	2.3	2/16/2004	11:57	3
2/16/2004	11:16	2.4	2/16/2004	11:58	3.9
2/16/2004	11:17	2.4	2/16/2004	11:59	2.9
2/16/2004	11:18	2.5	2/16/2004	12:00	2.9
2/16/2004	11:19	2.6	2/16/2004	12:01	3
2/16/2004	11:20	2.4	2/16/2004	12:02	3.1
2/16/2004	11:21	2.4	2/16/2004	12:03	2.7
2/16/2004	11:22	2.2	2/16/2004	12:04	4.9
2/16/2004	11:23	2.3	2/16/2004	12:05	2.3
2/16/2004	11:24	2.3	Final Average*		2.6
2/16/2004	11:25	2.3	Maximum*		4.9
2/16/2004	11:26	2.4	Minimum*		2.1
2/16/2004	11:27	2.3			
2/16/2004	11:28	2.2	*Does not include l	Invalid Av	eraging Periods
2/16/2004	11:29	2.1			

2.1

2.3 3.5

2.3

2.9

2.4

2.6

2.6

2.3

2.2

2.2

2.4

2.3

2/16/2004

2/16/2004

2/16/2004

2/16/2004

2/16/2004

2/16/2004

2/16/2004

2/16/2004

2/16/2004

2/16/2004

2/16/2004

2/16/2004

2/16/2004

11:30

11:31

11:32

11:33

11:34

11:35

11:36

11:37

11:38

11:39

11:40

11:41

11:42

s ("N/A")

Company: Okeelanta CoGen

Period Start: 02/16/2004

Plant:

Period End:

02/16/2004 13:49

12:47

City/St: South Bay, FL

Validation Type: Averaging Period: 1/1 min

Source: Stack 1

2/16/2004

13:28

2.7

ging Period: 1 min

		Average Opacity_1			Average Opacity_1
Period Start	•	%	Period Start		%
2/16/2004	12:47	2.4	2/16/2004	13:29	2.4
2/16/2004	12:48	2.3	2/16/2004	13:30	2.6
2/16/2004	12:49	2.6	2/16/2004	13:31	2.5
2/16/2004	12:50	2.5	2/16/2004	13:32	2.7
2/16/2004	12:51	2.3	2/16/2004	13:33	2.5
2/16/2004	12:52	2.3	2/16/2004	13:34	2.4
2/16/2004	12:53	2.3	2/16/2004	13:35	2.4
2/16/2004	12:54	2.2	2/16/2004	13:36	2.3
2/16/2004	12:55	2.1	2/16/2004	13:37	2.4
2/16/2004	12:56	2.3	2/16/2004	13:38	2.4
2/16/2004	12:57	2.3	2/16/2004	13:39	2.6
2/16/2004	12:58	2.3	2/16/2004	13:40	2.3
2/16/2004	12:59	2.3	2/16/2004	13:41	2.5
2/16/2004	13:00	2.3	2/16/2004	13:42	2.5
2/16/2004	13:01	2.3	2/16/2004	13:43	2.6
2/16/2004	13:02	2.2	2/16/2004	13:44	4.2
2/16/2004	13:03	2.2	2/16/2004	13:45	2.5
2/16/2004	13:04	2.3	2/16/2004	13:46	2.3
2/16/2004	13:05	2.4	2/16/2004	13:47	2.2
2/16/2004	13:06	2.4	2/16/2004	13:48	2.7
2/16/2004	13:07	2.3	2/16/2004	13:49	9.5
2/16/2004	13:08	2.3	Final Average*	_	2.5
2/16/2004	13:09	2.4	Maximum*		9.5
2/16/2004	13:10	2.2	Minimum*		2.1
2/16/2004	13:11	2.2			
2/16/2004	13:12	2.2	*Does not include l	nvalid Ave	raging Periods ("N/A")
2/16/2004	13:13	2.3			<i>8 8</i> ()
2/16/2004	13:14	2.3			•
2/16/2004	13:15	2.3			
2/16/2004	13:16	2.3			
2/16/2004	13:17	2.3			
2/16/2004	13:18	2.4			
2/16/2004	13:19	2.5			
2/16/2004	13:20	2.6			
2/16/2004	13:21	2.3			
2/16/2004	13:22	2.4			
2/16/2004	13:23	2.3			•
2/16/2004	13:24	2.3	•		
2/16/2004	13:25	2.3			•
2/16/2004	13:26	2.4		•	
2/16/2004	13:27	2.6			
0/1/6/0004	10.00	O : m			

Company: Okeelanta CoGen

Period Start:

02/13/2004 08:52

Plant:

Period End:

02/13/2004 09:54

City/St:

South Bay, FL

Validation Type:

1/1 min

Source:

2/13/2004

9:33

7

Averaging Period:

1 min

Stack 2

Type:

Block Avg

		Average			verage
	C	pacity_1		. 0	pacity_1
Period Start		%	Period Start		%
2/13/2004	8:52	5.7	2/13/2004	9:34	7.1
2/13/2004	8:53	5.8	2/13/2004	9:35	7.9
2/13/2004	8:54	5.9	2/13/2004	9:36	6.8
2/13/2004	8:55	5.6	2/13/2004	9:37	6.8
2/13/2004	8:56	6	2/13/2004	9:38	8
2/13/2004	8:57	5.9	2/13/2004	9:39	7.6
2/13/2004	8:58	5.8	2/13/2004	9:40	7.6
2/13/2004	8:59	5.8	2/13/2004	9:41	7.3
2/13/2004	9:00	5.9	2/13/2004	9:42	7.6
2/13/2004	9:01	5.5	2/13/2004	9:43	7.4
2/13/2004	9:02	5.7	2/13/2004	9:44	6.7
2/13/2004	9:03	6	2/13/2004	9:45	7.4
2/13/2004	9:04	6	2/13/2004	9:46	7.1
2/13/2004	9:05	5.8	2/13/2004	9:47	6.7
2/13/2004	9:06	5.8	2/13/2004	9:48	6.6
2/13/2004	9:07	6.2	2/13/2004	9:49	12.2
2/13/2004	9:08	6.3	2/13/2004	9:50	6.7
2/13/2004	9:09	6.2	2/13/2004	9:51	20.4
2/13/2004	9:10	6.4	2/13/2004	9:52	27.1
. 2/13/2004	9:11	6.1	2/13/2004	9:53	12.9
2/13/2004	9:12	6.4	2/13/2004	9:54	13
2/13/2004	9:13	5.9	Final Average*	_	7.3
2/13/2004	9:14	6.1	Maximum*		27.1
2/13/2004	9:15	6.4	Minimum*		5.5
2/13/2004	9:16	6.1			
2/13/2004	9:17	6	*Does not include Is	nvalid Avera	ging Perio
2/13/2004	9:18	6.1			0-0
2/13/2004	9:19	6			
2/13/2004	9:20	5.9			
2/13/2004	9:21	6.1			
2/13/2004	9:22	6.2			
2/13/2004	9:23	6.8			
2/13/2004	9:24	6	•		
2/13/2004	9:25	6.3			
2/13/2004	9:26	6.6			
2/13/2004	9:27	6.4			
2/13/2004	9:28	6.4			
2/13/2004	9:29	6.7			
2/13/2004	9:30	6.8			
2/13/2004	9:31	6.8			
2/13/2004	9:32	6.7			
2/12/2004	0.22	7			

Company: Okeelanta CoGen Period Start:

02/13/2004

12:40

Plant:

Period End:

02/13/2004 13:44

City/St:

South Bay, FL

Validation Type:

1/1 min

Source:

Stack 2

Averaging Period:

1 min

		verage pacity 1			Average Opacity 1
Period Start	_	%	Period Start		%
2/13/2004	12:40	4.8	2/13/2004	13:22	5.5
2/13/2004	12:41	5	2/13/2004	13:23	5.6
2/13/2004	12:42	5	2/13/2004	13:24	6.6
2/13/2004	12:43	5.2	2/13/2004	13:25	5.8
2/13/2004	12:44	5	. 2/13/2004	13:26	5.3
2/13/2004	12:45	5.1	2/13/2004	13:27	5.4
2/13/2004	12:46	4.9	2/13/2004	13:28	5.5
2/13/2004	12:47	4.8	2/13/2004	13:29	5.6
2/13/2004	12:48	5.9	2/13/2004	13:30	5.6
2/13/2004	12:49	5.7	2/13/2004	13:31	7
2/13/2004	12:50	5	2/13/2004	13:32	6
2/13/2004	12:51	5.1	2/13/2004	13:33	6
2/13/2004	12:52	5.8	2/13/2004	13:34	5.4
2/13/2004	12:53	6	2/13/2004	13:35	5.5
2/13/2004	12:54	5.1	2/13/2004	13:36	5.4
2/13/2004	12:55	4.9	2/13/2004	13:37	5.5
2/13/2004	12:56	5.1	2/13/2004	13:38	5.6
2/13/2004	12:57	5.2	2/13/2004	13:39	5.2
2/13/2004	12:58	. 5	2/13/2004	13:40	5.6
2/13/2004	12:59	5	2/13/2004	13:41	5.8
2/13/2004	13:00	4.9	2/13/2004	13:42	5.3
2/13/2004	13:01	5.3	2/13/2004	13:43	5.4
2/13/2004	13:02	5.1	Final Average*		5.5
2/13/2004	13:03	5.1	Maximum*		8
2/13/2004	13:04	6.3	Minimum*		4.8
2/13/2004	13:05	5.5			
2/13/2004	13:06	5.3	*Does not include I	nvalid Avera	aging Periods ("N/A")
2/13/2004	13:07	6.2	7		
2/13/2004	13:08	8			
2/13/2004	13:09	5.5			
2/13/2004	13:10	5.3			
2/13/2004	13:11	5.3			
2/13/2004	13:12	5.5			
2/13/2004	13:13	5.5			
2/13/2004	13:14	5.3			
2/13/2004	13:15	5.6			
2/13/2004	13:16	5.5			
2/13/2004	13:17	5.2	•		
2/13/2004	13:18	5.2			
2/13/2004	13:19	7.9			
2/13/2004	13:20	6.2			
2/13/2004	13:21	6.6	•		

Company: Okeelanta CoGen Period Start: 02/13/2004

Plant:

Period End: 02/13/2004

Validation Type:

15:32

14:27

City/St:

2/13/2004

15:08

6.1

South Bay, FL

1/1 min Averaging Period: 1 min

Source: Stack 2

Block Avg Type:

•		Average		•		Average	
		Opacity 1			Opacity 1		
Per	iod Start	. •	%	Period Start		%	
	2/13/2004	14:27	6.8	2/13/2004	15:09	6	
	2/13/2004	14:28	8.3	2/13/2004	15:10	7	
	2/13/2004	14:29	6.2	2/13/2004	15:11	6	
	2/13/2004	14:30	8.6	2/13/2004	15:12	6.7	
	2/13/2004	14:31	5.4	2/13/2004	15:13	5.8	
	2/13/2004	14:32	5.1	2/13/2004	15:14	6.6	
	2/13/2004	14:33	5.7	2/13/2004	15:15	6	
	2/13/2004	14:34	5.8	2/13/2004	15:16	6.5	
	2/13/2004	14:35	5.5	2/13/2004	15:17	6	
	2/13/2004	14:36	5.6	2/13/2004	15:18	5.9	
	2/13/2004	14:37	5.4	2/13/2004	15:19	6.3	
	2/13/2004	14:38	5.7	2/13/2004	15:20	7.6	
	2/13/2004	14:39	6.3	2/13/2004	15:21	6.6	
	2/13/2004	14:40	5.6	2/13/2004	15:22	6.5	
	2/13/2004	14:41	5.7	2/13/2004	15:23	6.4	
	2/13/2004	14:42	5.5	2/13/2004	15:24	6.2	
	2/13/2004	14:43	6	` 2/13/2004	15:25	5.8	
	2/13/2004	14:44	5.5	2/13/2004	15:26	5.9	
	2/13/2004	14:45	5.7	2/13/2004	15:27	6.1	
	2/13/2004	14:46	5.6	2/13/2004	15:28	11	
	2/13/2004	14:47	5.8	2/13/2004	15:29	6.6	
	2/13/2004	14:48	5.9	2/13/2004	15:30	6.7	
	2/13/2004	14:49	5.8	2/13/2004	15:31	13.6	
*	2/13/2004	14:50	6.2	2/13/2004	15:32	6.4	
	2/13/2004	14:51	6.2	Final Average*		6.5	
	2/13/2004	14:52	5.9	Maximum*		16.4	
	2/13/2004	14:53	5.8	Minimum*		5.1	
	2/13/2004	14:54	5.5				
	2/13/2004	14:55	5.5	*Does not include I	nvalid Aver	aging Periods ("N/	
	2/13/2004	14:56	5.5				
	2/13/2004	İ4:57	5.9				
	2/13/2004	14:58	5.9				
	2/13/2004	14:59	5.8				
	2/13/2004	15:00	7.1				
	2/13/2004	15:01	6.2				
	2/13/2004	15:02	5.7				
	2/13/2004	15:03	6				
	2/13/2004	15:04	6.1				
	2/13/2004	15:05	6.7				
	. 2/13/2004	15:06	5.8				
	2/13/2004	15:07	6.3				
	0/12/0004	15.00					

Company: Okeelanta CoGen

Period Start: 02/11/2004

09:50

Plant:

2/11/2004

2/11/2004

2/11/2004

10:29

10:30

10:31

Period End:

02/11/2004 10:54

City/St:

South Bay, FL

Validation Type:

1/1 min

Source: Stack 3

Averaging Period:

Period: 1 min
Type: Block Avg

		verage pacity 1			Average Opacity 1
Period Start		%	Period Start		%
2/11/2004	9:50	5.9	2/11/2004	10:32	5.9
2/11/2004	9:51	5.9	2/11/2004	10:33	6
2/11/2004	9:52	5.9	2/11/2004	10:34	5.9
2/11/2004	9:53	5.8	2/11/2004	10:35	5.9
2/11/2004	9:54	5.9	2/11/2004	10:36	5.9
2/11/2004	9:55	5.8	2/11/2004	10:37	5.9
2/11/2004	9:56	5.9	2/11/2004	10:38	5.9
2/11/2004	9:57	5.9	2/11/2004	10:39	. 6
2/11/2004	9:58	5.9	2/11/2004	10:40	6
2/11/2004	9:59	6	2/11/2004	10:41	6
2/11/2004	10:00	5.9	2/11/2004	10:42	6
2/11/2004	10:01	5.9	2/11/2004	10:43	6
2/11/2004	10:02	5.9	2/11/2004	10:44	6
2/11/2004	10:03	5.9	2/11/2004	10:45	6
2/11/2004	10:04	6.2	2/11/2004	10:46	6.1
2/11/2004	10:05	6.1	2/11/2004	10:47	6.1
2/11/2004	10:06	6	2/11/2004	10:48	6
2/11/2004	10:07	5.9	2/11/2004	10:49	5.9
2/11/2004	10:08	6	2/11/2004	10:50	7.2
2/11/2004	10:09	6	2/11/2004	10:51	6.3
2/11/2004	10:10	6.1	2/11/2004	10:52	6.5
2/11/2004	10:11	6	2/11/2004	10:53	7.9
2/11/2004	10:12	6.1	2/11/2004	10:54	9.6
2/11/2004	10:13	6	Final Average*	. —	6.1
2/11/2004	10:14	6	Maximum*		9.6
2/11/2004	10:15	6.1	Minimum*		5.8
2/11/2004	10:16	6			•
2/11/2004	10:17	. 6	*Does not include I	nvalid Aver	aging Periods ("N/A
2/11/2004	10:18	6.1			
2/11/2004	10:19	6.1			
2/11/2004	10:20	6			
2/11/2004	10:21	6			
2/11/2004	10:22	5.9			
2/11/2004	10:23	5.9			
2/11/2004	10:24	6			
2/11/2004	10:25	5.9			
2/11/2004	10:26	6			
2/11/2004	10:27	6			
2/11/2004	10:28	6			
0/11/0004	10.00	~ ·	· ·		

5.9

5.9

6

Company: Okeelanta CoGen

Period Start:

02/11/2004 11:36

Plant:

Period End:

02/11/2004 12:42

City/St:

South Bay, FL

Validation Type:

1/1 min

Source:

Averaging Period:

1 min

Stack 3

Type:

Block Avg

		verage pacity_1			verage pacity_1	
Period Start		%	Period Start		%	
2/11/2004	11:36	6.2	2/11/2004	12:18	5.5	
2/11/2004	11:37	5.9	2/11/2004	12:19	5.6	
2/11/2004	11:38	6	2/11/2004	12:20	5.5	
2/11/2004	11:39	6	2/11/2004	12:21	5.5	
2/11/2004	11:40	5.9	2/11/2004	12:22	5.5	
2/11/2004	11:41	5.9	2/11/2004	12:23	5.8	
2/11/2004	11:42	5.9	2/11/2004	12:24	5.6	
2/11/2004	11:43	5.9	2/11/2004	12:25	5.4	
2/11/2004	11:44	5.7	2/11/2004	12:26	5.5	
2/11/2004	11:45	5.8	2/11/2004	12:27	5.6	
2/11/2004	11:46	5.8	2/11/2004	12:28	5.5	
2/11/2004	11:47	5.8	2/11/2004	12:29	5.5	
2/11/2004	11:48	5.6	2/11/2004	12:30	5.4	
2/11/2004	11:49	5.6	2/11/2004	12:31	5.3	
2/11/2004	11:50	5.7	2/11/2004	12:32	5.4	
2/11/2004	11:51	5.6	2/11/2004	12:33	5.5	
2/11/2004	11:52	5.5	2/11/2004	12:34	5.6	
2/11/2004	11:53	5.5	2/11/2004	12:35	5.4	
2/11/2004	11:54	5.5	2/11/2004	12:36	6.6	
2/11/2004	11:55	5.6	2/11/2004	12:37	5.7	
2/11/2004	11:56	5.5	2/11/2004	12:38	6.4	
2/11/2004	11:57	5.5	2/11/2004	12:39	6.3	
2/11/2004	11:58	5.5	2/11/2004	12:40	6.3	
2/11/2004	11:59	5.5	2/11/2004	12:41	5.8	
2/11/2004	12:00	5.4	2/11/2004	12:42	8.8	
2/11/2004	12:01	5.6	Final Average*		5.7	
2/11/2004	12:02	5.6	Maximum*		8.8	
2/11/2004	12:03	5.6	Minimum*		5.3	
2/11/2004	12:04	5.7				
2/11/2004	12:05	5.6	*Does not include I	nvalid Avera	ging Periods ("	'N/A")
2/11/2004	12:06	5.6				,
2/11/2004	12:07	5.7				
2/11/2004	12:08	5.5				•
2/11/2004	12:09	5.7			•	
2/11/2004	12:10	5.6	5.			
2/11/2004	12:11	5.6				
2/11/2004	12:12	5.6	· ·			
2/11/2004	12:13	5.7				
2/11/2004	12:14	5.5		•		
2/11/2004	12:15	5.7				
2/11/2004	12:16	5.5	•			
2/11/2004	12:17	5.5				

Company: Okeelanta CoGen Period Start: 02/11/2004

13:20

Plant:

2/11/2004

2/11/2004

2/11/2004

2/11/2004

2/11/2004

2/11/2004

2/11/2004

2/11/2004

2/11/2004

2/11/2004

2/11/2004

13:51

13:52

13:53

13:54

13:55

13:56

13:57

13:58

13:59

14:00

14:01

South Bay, FL

Period End: Validation Type:

02/11/2004 14:25

City/St: Source: Stack 3

Averaging Period:

1/1 min 1 min

Type: Block Avg

		verage pacity_1			Average Opacity_1
Period Start		%	Period Start		%
2/11/2004	13:20	5.6	2/11/2004	14:02	5.8
2/11/2004	13:21	5.6	2/11/2004	14:03	5.7
2/11/2004	13:22	5.5	2/11/2004	14:04	5.5
2/11/2004	13:23	5.5	2/11/2004	14:05	5.7
2/11/2004	13:24	5.6	2/11/2004	14:06	5.6
2/11/2004	13:25	5.5	2/11/2004	14:07	5.6
2/11/2004	13:26	5.5	2/11/2004	14:08	5.5
2/11/2004	13:27	5.5	2/11/2004	14:09	5.5
2/11/2004	13:28	5.5	2/11/2004	14:10	5.5
2/11/2004	13:29	5.6	2/11/2004	14:11	5.6
2/11/2004	13:30	5.5	2/11/2004	14:12	6.2
2/11/2004	13:31	5.5	2/11/2004	14:13	6.1
2/11/2004	13:32	5.5	2/11/2004	14:14	5.8
2/11/2004	13:33	5.6	2/11/2004	14:15	5.8
2/11/2004	13:34	5.5	2/11/2004	14:16	5.6
2/11/2004	13:35	5.5	2/11/2004	14:17	5.5
2/11/2004	13:36	5.5	2/11/2004	14:18	5.8
2/11/2004	13:37	5.5	2/11/2004	14:19	5.5
2/11/2004	13:38	5.5	2/11/2004	14:20	6.8
2/11/2004	13:39	5.5	2/11/2004	14:21	6
2/11/2004	13:40	5.5	2/11/2004	14:22	5.9
2/11/2004	13:41	5.5	2/11/2004	14:23	5.9
2/11/2004	13:42	5.5	2/11/2004	14:24	9.3
2/11/2004	13:43	5.4	2/11/2004	14:25	6.1
2/11/2004	13:44	5.4	Final Average*		5.7
2/11/2004	13:45	5.5	Maximum*		9.3
2/11/2004	13:46	5.5	Minimum*		5.4
2/11/2004	13:47	5.4			
2/11/2004	13:48	5.5	*Does not include I	nvalid Av	eraging Periods
2/11/2004	13:49	5.5			5 0
2/11/2004	13:50	5.5			

5.5

5.5

5.7

5.5 5.7

5.5

5.5

5.5

5.5

5.6

s ("N/A")

Company: Plant: City/St: Source: Okeelanta CoGen

Period Start:

01/22/03 01/22/03 09:43 Period End: 11:42 1/1 min

South Bay, FL Stack 1

1/22/2003

10:46

2.4

Validation Type: Averaging Period: Type: l min Block Avg

		Average pacity_1			Average Opacity_1
Period Start.		%	Period Start		<u>%</u>
1/22/2003	9:43	2.3	1/22/2003	10:47	5
1/22/2003	9:44	2.3	1/22/2003	10:48	3.1
1/22/2003	9:45	2.3	1/22/2003	10:49	2.4
1/22/2003	9:46	2.2	1/22/2003	10:50	2.6
1/22/2003	9:47	2.3	1/22/2003	10:51	2.3
1/22/2003	9:48	2.3	1/22/2003	10:52	2.7
1/22/2003	9:49	2.3	1/22/2003	10:53	2.6
1/22/2003	9:50	2.2	1/22/2003	10:54	2.2
1/22/2003	9:51	2.2	1/22/2003	10:55	2.1
1/22/2003	9:52	2.3	1/22/2003	10:56	2.2
1/22/2003	9:53 9:54	2.3	1/22/2003	10:57	2.1 2.2
1/22/2003	9:54 9:55	2.3 2.2	1/22/2003 1/22/2003	10:58 10:59	2.2
1/22/2003 1/22/2003	9:56 .	2.2	1/22/2003	11:00	2.1
1/22/2003	9:57	2.1	1/22/2003	11:01	2.3
1/22/2003	9:58	2.2	1/22/2003	11:02	2.1
1/22/2003	9:59	3.1	1/22/2003	11:02	2.3
1/22/2003	10:00	2.7	1/22/2003	11:04	2.1
1/22/2003	10:01	2.4	1/22/2003	11:05	2.3
1/22/2003	10:02	2.2	1/22/2003	11:06	2.2
1/22/2003	10:03	2.3	1/22/2003	11:07	2.1
1/22/2003	10:04	2.3	1/22/2003	11:08	2.3
1/22/2003	10:05	2.4	1/22/2003	11:09	2.1
1/22/2003	10:06	2.3	1/22/2003	11:10	2.4
1/22/2003	10:07	2.1	1/22/2003	11:11	2.3
1/22/2003	10:08	2	1/22/2003	11:12	2.2
1/22/2003	10:09	2	1/22/2003	11:13	2
1/22/2003	10:10	2	1/22/2003	11:14	2.3
1/22/2003	10:11	1.9	1/22/2003	11:15	2.3
1/22/2003	10:12	1.9	1/22/2003	11:16	2.5
1/22/2003	10:13	1.9	1/22/2003	11:17	2.4
1/22/2003	10:14	1.9	1/22/2003	11:18	2.5
1/22/2003	10:15	2	1/22/2003	11:19	2.6
1/22/2003	10:16	2.1	1/22/2003	11:20	2.4
1/22/2003	10:17	2.3	1/22/2003	11:21	2.6
1/22/2003	10:18	2.3	1/22/2003	11:22	2.3
1/22/2003	10:19	2.2	1/22/2003	11:23	2.4
1/22/2003	10:20	2.1	1/22/2003	11:24	2.5
1/22/2003	10:21	5.3	1/22/2003	11:25	2.3
1/22/2003	10:22	6.3	1/22/2003	11:26	2.3
1/22/2003	10:23	2.6	1/22/2003	11:27	2.3
1/22/2003	10:24	2.1	1/22/2003	11:28	2.4
1/22/2003	10:25	2.2	1/22/2003	11:29	2.6
1/22/2003	10:26	2.3	1/22/2003	11:30	2.4
1/22/2003	10:27	2.4	1/22/2003	11:31	2.4
1/22/2003	10:28	6.5	1/22/2003	11:32	2.4
1/22/2003	10:29	3	1/22/2003	11:33	2.4
1/22/2003	10:30	2.5	1/22/2003	11:34	2.3
1/22/2003	10:31	3.1	1/22/2003	11:35	2.3
1/22/2003	10:32	13.5	1/22/2003	11:36	2.2
1/22/2003	10:33	33.1	1/22/2003	11:37	2.1
1/22/2003	10:34	25.8	1/22/2003	11:38	2.5
1/22/2003	10:35	24.8	1/22/2003	11:39	2.2
1/22/2003	10:36	16.6	1/22/2003	11:40	5.4
1/22/2003	10:37	11.3	1/22/2003	11:41	3.9
1/22/2003	10:38	4.6	1/22/2003	11:42	3.5
1/22/2003	10:39	3.1	Final Average*		3.4
1/22/2003	10:40	3	Maximum*		33.1
1/22/2003	10:41	2.7	Minimum*		1.9
1/22/2003	10:42	3		_	
1/22/2003	10:43	2.8	*Does not include	Invalid A	veraging Periods (")
1/22/2003	10:44	2.3			
1/22/2003	10:45 10:46	2.2			
177777003	111.46	14			

Company: Okeelanta CoGen

Period Start:

01/22/03

12:17

Plant:

South Bay, FL

Period End: Validation Type:

01/22/03 1/1 min 13:20

City/St: Source:

1/22/2003

1/22/2003

12:57

12:58

2.3

2.3

Stack 1

Averaging Period:

1 min

eriod: 1 min

		Average Opacity 1			verage pacity 1
Period Start		%	Period Start	O ,	%
1/22/2003	12:17	2.3	1/22/2003	12:59	2.2
1/22/2003	12:18	2.1	1/22/2003	13:00	2.3
1/22/2003	12:19	2.4	1/22/2003	13:01	2.3
1/22/2003	12:20	2.4	1/22/2003	13:02	2.3
1/22/2003	12:21	2.3	1/22/2003	13:03	2.4
1/22/2003	12:22	2.3	1/22/2003	13:04	2.8
1/22/2003	12:23	2.3	1/22/2003	13:05	2.4
1/22/2003	12:24	2.4	1/22/2003	13:06	2.4
1/22/2003	12:25	2.5	1/22/2003	13:07	2.4
1/22/2003	12:26	2.5	1/22/2003	13:08	2.4
1/22/2003	12:27	2.6	1/22/2003	13:09	2.5
1/22/2003	12:28	2.3	1/22/2003	13:10	2.2
1/22/2003	12:29	2.3	1/22/2003	13:11	2.3
1/22/2003	12:30	2.3	1/22/2003	13:12	2.3
1/22/2003	12:31	2.2	1/22/2003	13:13	2.4
1/22/2003	12:32	2.2	1/22/2003	13:14	2.2
1/22/2003	12:33	2.1	1/22/2003	13:15	2.8
1/22/2003	12:34	2.1	1/22/2003	13:16	2.6
1/22/2003	12:35	2.2	1/22/2003	13:17	2.6
1/22/2003	12:36	2.3	1/22/2003	13:18	4.2
1/22/2003	12:37	2.7	1/22/2003	13:19	2.4
1/22/2003	12:38	2.4	1/22/2003	13:20	2.4
1/22/2003	12:39	2.3	Final Average*		2.4
1/22/2003	12:40	2.5	Maximum*		4.2
1/22/2003	12:41	2.6	Minimum*		2.1
1/22/2003	12:42	2.6			
1/22/2003	12:43	2.7	*Does not include l	nvalid Avera	ging Period
1/22/2003	12:44	2.9			0 0
1/22/2003	12:45	2.6			
1/22/2003	12:46	2.5			
1/22/2003	12:47	2.4			
1/22/2003	12:48	2.4			
1/22/2003	12:49	2.3	,		
1/22/2003	12:50	2.4			
1/22/2003	12:51	2.4			
1/22/2003	12:52	2.5			
1/22/2003	12:53	2.5	•		
1/22/2003	12:54	2.4			
1/22/2003	12:55	2.5			
1/22/2003	12:56	2.4	·	•	
1/22/2002	10.57	2.2			

Company:

Okeelanta CoGen

Period Start:

01/22/03

14:03

Plant:

1/22/2003

1/22/2003

1/22/2003

1/22/2003

1/22/2003

1/22/2003

1/22/2003

1/22/2003

1/22/2003

1/22/2003

1/22/2003

1/22/2003

1/22/2003

1/22/2003

14:31

14:32

14:33

14:34

14:35

14:36

14:37

14:38

14:39

14:40

14:41

14:42

14:43

14:44

South Bay, FL

Period End: Validation Type: 01/22/03 1/1 min

15:06

City/St: Source:

1 min

Stack 1-

Averaging Period:

Type: Block Avg

		Average Opacity_1			Average Opacity_1
Period Start		%	Period Start		%
1/22/2003	14:03	2	1/22/2003	14:45	. 2
1/22/2003	14:04	2.3	1/22/2003	14:46	2.1
1/22/2003	14:05	2	1/22/2003	14:47	2.2
1/22/2003	14:06	2	1/22/2003	14:48	2.2
1/22/2003	14:07	2	1/22/2003	14:49	2.1
1/22/2003	14:08	1.9	1/22/2003	14:50	2.3
1/22/2003	14:09	1.9	1/22/2003	14:51	2.1
1/22/2003	14:10	2	1/22/2003	14:52	2.2
1/22/2003	14:11	2	1/22/2003	14:53	2
1/22/2003	14:12	2	1/22/2003	14:54	1.9
1/22/2003	14:13	2.3	1/22/2003	14:55	2.3
1/22/2003	14:14	2.2	1/22/2003	14:56	2.2
1/22/2003	14:15	2.2	1/22/2003	14:57	2.2
1/22/2003	14:16	2	1/22/2003	14:58	2.1
1/22/2003	14:17	2	1/22/2003	14:59	2.1
1/22/2003	14:18	2	1/22/2003	15:00	2
1/22/2003	14:19	2.2	1/22/2003	15:01	2.6
1/22/2003	14:20	2.1	1/22/2003	15:02	2.2
1/22/2003	14:21	2.3	1/22/2003	15:03	2.3
1/22/2003	14:22	2	1/22/2003	15:04	8.1
1/22/2003	14:23	2	1/22/2003	15:05	2.8
1/22/2003	14:24	2	1/22/2003	15:06	2.5
1/22/2003	14:25	2	Final Average*		2.2
1/22/2003	14:26	1.9	Maximum*	•	8.1
1/22/2003	14:27	1.9	Minimum*		1.8
1/22/2003	14:28	1.8			
1/22/2003	14:29	1.9	*Does not include l	nvalid Ave	eraging Periods
1/22/2003	14:30	2	,	•	

1.9

1.9

1.9 2

2.1

2.2

2.2

2.3

2.1

2

2 2

2.1

2

s ("N/A")

Company: Okeelanta CoGen Period Start: 01/23/03 10:58

Plant:

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

11:32

11:33

11:34

11:35

11:36

11:37

11:38

11:39

3.8

3.7

3.6

3.7

3.6

3.8

3.8

3.6

Period End:

01/23/03 12:01

City/St: South Bay, FL Source:

Validation Type:

 $1/1 \min$

Averaging Period:

1 min

Stack 2

Block Avg Type:

		verage pacity 1			Average pacity_1
Period Start		%	Period Start		%
1/23/2003	10:58	3.6	1/23/2003	11:40	3.9
1/23/2003	10:59	3.7	1/23/2003	11:41	3.8
1/23/2003	11:00	3.6	1/23/2003	11:42	3.7
1/23/2003	11:01	3.6	1/23/2003	11:43	4
1/23/2003	11:02	3.8	1/23/2003	11:44	4
1/23/2003	11:03	3.7	1/23/2003	11:45	3.8
1/23/2003	. 11:04	4	1/23/2003	11:46	3.6
1/23/2003	11:05	3.6	1/23/2003	11:47	3.7
1/23/2003	11:06	3.6	1/23/2003	11:48	3.6
1/23/2003	11:07	3.7	1/23/2003	11:49	3.6
1/23/2003	11:08	4.9	1/23/2003	11:50	3.6
1/23/2003	11:09	3.7	1/23/2003	11:51	3.6
1/23/2003	11:10	3.7	1/23/2003	11:52	4.1
1/23/2003	11:11	3.6	1/23/2003	11:53	3.6
1/23/2003	11:12	3.6	1/23/2003	11:54	3.7
1/23/2003	11:13	3.6	1/23/2003	11:55	. 3.6
1/23/2003	11:14	3.6	1/23/2003	11:56	3.6
1/23/2003	11:15	3.7	1/23/2003	11:57	3.6
1/23/2003	11:16	3.7	1/23/2003	11:58	3.9
1/23/2003	11:17	3.6	1/23/2003	11:59	3.7
1/23/2003	11:18	3.9	1/23/2003	12:00	3.6
1/23/2003	11:19	3.6	1/23/2003	12:01	4.1
1/23/2003	11:20	3.6	Final Average*		3.7
1/23/2003	11:21	3.6	Maximum*		4.9
1/23/2003	11:22	3.7	Minimum*		3.6
1/23/2003	11:23	3.7			
1/23/2003	11:24	3.8	*Does not include I	nvalid Avera	aging Periods ("N/A"
1/23/2003	11:25	3.7			- , ,
1/23/2003	11:26	3.8			
1/23/2003	11:27	3.8			
1/23/2003	11:28	3.8			
1/23/2003	11:29	3.7			
1/23/2003	11:30	3.7			
1/23/2003	11:31	3.8			
1 /00 /000					

Company: Okeelanta CoGen Period Start: 01/23/03 12:31

Plant:

Period End: 01/23/03 13:34

City/St: Source: Stack 2

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

12:59

13:00

13:01

13:02

13:03

13:04

13:05

13:06

13:07

13:08

13:09

13:10

13:11

13:12

South Bay, FL

Validation Type:

1/1 min

Averaging Period:

1 min

Type:

Block Avg

		Average Opacity 1	•		Average Opacity_1
Period Start	Ì	%	Period Start		%
1/23/2003	12:31	3.6	1/23/2003	13:13	3.7
1/23/2003	12:32	3.6	1/23/2003	13:14	3.6
1/23/2003	12:33	3.6	1/23/2003	13:15	3.7
1/23/2003	12:34	3.6	1/23/2003	13:16	3.7
1/23/2003	12:35	3.5	1/23/2003	13:17	3.8
1/23/2003	12:36	3.6	1/23/2003	13:18	3.7
1/23/2003	12:37	3.5	1/23/2003	13:19	3.6
1/23/2003	12:38	3.6	1/23/2003	13:20	3.7
1/23/2003	12:39	3.6	1/23/2003	13:21	3.6
1/23/2003	12:40	3.6	1/23/2003	13:22	3.6
1/23/2003	12:41	3.6	1/23/2003	13:23	3.6
1/23/2003	12:42	3.6	1/23/2003	13:24	3.5
1/23/2003	12:43	3.6	1/23/2003	13:25	3.5
1/23/2003	12:44	3.6	1/23/2003	13:26	3.6
1/23/2003	12:45	3.6	1/23/2003	13:27	3.6
1/23/2003	12:46	3.6	1/23/2003	13:28	4.2
1/23/2003	12:47	3.6	1/23/2003	13:29	7.5
1/23/2003	12:48	3.6	1/23/2003	13:30	6.2
1/23/2003	12:49	3.5	1/23/2003	13:31	7
.1/23/2003	12:50	3.5	1/23/2003	13:32	4.8
1/23/2003	12:51	3.6	1/23/2003	13:33	4.2
1/23/2003	12:52	3.5	1/23/2003	13:34	4.4
1/23/2003	12:53	3.6	Final Average*		3.8
1/23/2003	12:54	3.5	Maximum*		7.5
1/23/2003	12:55	3.5	Minimum*		3.4
1/23/2003	12:56	3.6			
1/23/2003	12:57	3.6	*Does not include I	nvalid Av	eraging Period
1/23/2003	12:58	3.6	•		

3.4

3.6

3.5

3.6

3.5

3.6

3.5

3.6

3.5

3.6

3.8

4.8

3.7

ds ("N/A")

Company: Okeelanta CoGen

Period Start: 01/23/03

14:01

Plant:

Period End:

01/23/03 15:04

City/St:

South Bay, FL

Validation Type:

1/1 min 1 min

Source: Stack 2

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003

1/23/2003 1/23/2003 14:27

14:28

14:29

14:30

14:31

14:32

14:33

14:34

14:35

14:36

14:37

14:38

14:39

14:40

14:41

14:42

Averaging Period:

Type: Block Avg

	,	Average Opacity_1	·		Average Opacity_1
Period Start		%	Period Start		%
1/23/2003	14:01	3.3	1/23/2003	14:43	3.4
1/23/2003	14:02	3.3	1/23/2003	14:44	3.3
1/23/2003	14:03	3.5	1/23/2003	14:45	3.3
1/23/2003	14:04	3.3	1/23/2003	14:46	3.3
1/23/2003	14:05	3.2	1/23/2003	14:47	3.3
1/23/2003	14:06	3.5	1/23/2003	14:48	3.6
1/23/2003	14:07	3.5	1/23/2003	14:49	3.5
1/23/2003	14:08	3.7	1/23/2003	14:50	3.5
1/23/2003	14:09	3.6	1/23/2003	14:51	3.5
1/23/2003	14:10	3.7	1/23/2003	14:52	4.1
1/23/2003	14:11	3.7	1/23/2003	14:53	3.6
1/23/2003	14:12	3.8	1/23/2003	14:54	3.6
1/23/2003	14:13	3.7	1/23/2003	14:55	3.8
1/23/2003	14:14	3.6	1/23/2003	14:56	3.8
1/23/2003	14:15	3.4	1/23/2003	14:57	3.8
1/23/2003	14:16	3.4	1/23/2003	14:58	3.6
1/23/2003	14:17	3.4	1/23/2003	14:59	3.7
1/23/2003	14:18	3.4	1/23/2003	15:00	3.5
1/23/2003	14:19	3.6	1/23/2003	15:01	6.5
1/23/2003	14:20	3.4	1/23/2003	15:02	4
1/23/2003	14:21	3.4	1/23/2003	15:03	3.8
1/23/2003	14:22	3.4	1/23/2003	15:04	4.1
1/23/2003	14:23	3.4	Final Average*		3.5
1/23/2003	14:24	3.4	Maximum*		6.5
1/23/2003	14:25	3.3	Minimum*		3.1
1/23/2003	14:26	3.4			

3.3

3.6

3.6

3.5

3.6

3.4

3.2

3.2

3.1

3.1

3.1

3.3

3.3

3.3

-3.2

^{*}Does not include Invalid Averaging Periods ("N/A")

Company: Okeelanta CoGen Period Start: 01/21/03 12:16

Plant:

Period End: .01/21/03 13:21

City/St:

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003 1/21/2003

1/21/2003

12:46

12:47

12:48

12:49

12:50

12:51

12:52

12:53

12:54

12:55

12:56

12:57

South Bay, FL

Validation Type:

1/1 min 1 min

Source:

Stack 3

Averaging Period:

Type: Block Avg

		verage pacity_1			Average Opacity_1
Period Start		%	Period Start		%
1/21/2003	12:16	0.2	1/21/2003	12:58	-0.1
1/21/2003	12:17	0	1/21/2003	12:59	-0.1
1/21/2003	12:18	-0.1	1/21/2003	13:00	-0.1
1/21/2003	12:19	-0.1	1/21/2003	13:01	-0.2
1/21/2003	12:20	-0.1	1/21/2003	13:02	-0.2
1/21/2003	12:21	0	1/21/2003	13:03	-0.1
1/21/2003	12:22	0.1	1/21/2003	13:04	0.1
1/21/2003	12:23	-0.1	1/21/2003	13:05	0.1
1/21/2003	12:24	-0.1	1/21/2003	13:06	-0.2
1/21/2003	12:25	-0.1	1/21/2003	13:07	-0.1
1/21/2003	12:26	-0.1	1/21/2003	13:08	-0.1
1/21/2003	12:27	-0.2	1/21/2003	13:09	0
1/21/2003	12:28	0	1/21/2003	13:10	0.2
1/21/2003	12:29	-0.2	1/21/2003	13:11	-0.1
1/21/2003	12:30	-0.1	1/21/2003	13:12	0
1/21/2003	12:31	0	1/21/2003	13:13	0
1/21/2003	12:32	-0.1	1/21/2003	13:14	0.1
1/21/2003	12:33	-0.2	1/21/2003	13:15	0.1
1/21/2003	12:34	-0.1	1/21/2003	13:16	0.6
1/21/2003	12:35	-0.1	1/21/2003	13:17	-0.1
1/21/2003	12:36	0	1/21/2003	13:18	-0.1
1/21/2003	12:37	-0.2	1/21/2003	13:19	0
1/21/2003	12:38	-0.1	1/21/2003	13:20	0.3
1/21/2003	12:39	-0.1	1/21/2003	13:21	0.8
1/21/2003	12:40	-0.1	Final Average*		. 0
1/21/2003	12:41	-0.2	Maximum*		. 1
1/21/2003	12:42	-0.2	Minimum*		-0.3
1/21/2003	12:43	-0.2			
1/21/2003	12:44	-0.3	*Does not include l	nvalid Av	eraging Periods
1/21/2003	12:45	0.2	•		_

1

0

0

0

0

0.5

-0.1

-0.1

0.1

0.2

-0.1

ls ("N/A")

Company: Okeelanta CoGen

Period Start: 01/21/03

14:07 15:10

Plant:

01/21/03

City/St: South Bay, FL

14:31

14:32

14:33

14:34

14:35

14:36

14:37

14:38

14:39

14:40

14:41

14:42

14:43

14:44

14:45

14:46

14:47

14:48

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

1/21/2003

Validation Type:
Averaging Period:

Period End:

1/1 min 1 min

Source: Stack 3

Type: Block Avg

		Average			Average
	(Opacity_1			Opacity_1
Period Start	`	%	Period Start		%
1/21/2003	14:07	-0.1	1/21/2003	14:49	-0.3
1/21/2003	14:08	-0.1	1/21/2003	14:50	-0.4
1/21/2003	14:09	-0.2	1/21/2003	14:51	-0.4
1/21/2003	14:10	-0.1	1/21/2003	14:52	-0.3
1/21/2003	14:11	-0.1	1/21/2003	14:53	-0.3
1/21/2003	14:12	-0.2	1/21/2003	14:54	-0.4
1/21/2003	14:13	-0.2	1/21/2003	14:55	-0.4
1/21/2003	14:14	-0.1	1/21/2003	14:56	-0.4
1/21/2003	14:15	0.1	1/21/2003	14:57	-0.3
1/21/2003	14:16	-0.1	1/21/2003	14:58	-0.5
1/21/2003	14:17	-0.1	1/21/2003	14:59	-0.3
1/21/2003	14:18	0.2	1/21/2003	15:00	-0.4
1/21/2003	14:19	-0.2	1/21/2003	15:01	-0.3
1/21/2003	14:20	0.8	1/21/2003	15:02	-0.5
1/21/2003	14:21	. 0	1/21/2003	15:03	-0.4
1/21/2003	14:22	-0.3	1/21/2003	15:04	-0.2
1/21/2003	14:23	-0.3	1/21/2003	15:05	-0.3
1/21/2003	14:24	-0.3	1/21/2003	15:06	0
1/21/2003	14:25	0.1	1/21/2003	15:07	-0.3
1/21/2003	14:26	-0.1	1/21/2003	15:08	-0.2
1/21/2003	14:27	0.1	1/21/2003	15:09	0.3
1/21/2003	14:28	0	1/21/2003	15:10	-0.2
1/21/2003	14:29	-0.3	Final Average*	·	-0.2
1/21/2003	14:30	-0.2	Maximum*	.zv	0.8

-0.2

-0.1

-0.2

-0.3 0

-0.1

-0.2

-0.3

-0.2

-0.3

-0.2

-0.2

-0.3

-0.2

-0.4

-0.4

-0.3 -0.3 Minimum*

-0.5

^{*}Does not include Invalid Averaging Periods ("N/A")

Company: Okeelanta CoGen

Period Start: 01/21/03

16:13 17:24

Plant:

Period End:

01/21/03

City/St:

South Bay, FL

Validation Type:

1/1 min

Source:

Stack 3

Averaging Period:

Period: 1 min
Type: Block Avg

Average	Average
•	
	·

		verage			verage
	$\mathbf{O}_{\mathbf{i}}$	pacity_1		$O_{\mathbf{i}}$	pacity_1
Period Start		%	Period Start		%
1/21/2003	16:13	1.6	1/21/2003	16:55	0
1/21/2003	16:14	0.8	1/21/2003	16:56	0.1
. 1/21/2003	16:15	, 1.3	1/21/2003	16:57	0
1/21/2003	16:16	0.8	1/21/2003	16:58	0
1/21/2003	16:17	4	1/21/2003	16:59	-0.1
1/21/2003	16:18	4	1/21/2003	17:00	-0.2
1/21/2003	16:19	0.1	1/21/2003	17:01	-0.1
1/21/2003	16:20	-0.1	1/21/2003	17:02	0.2
1/21/2003	16:21	0	1/21/2003	17:03	-0.1
1/21/2003	16:22	-0.1	1/21/2003	17:04	-0.1
1/21/2003	16:23	-0.1	1/21/2003	17:05	-0.2
1/21/2003	16:24	0.1	1/21/2003	17:06	-0.1
1/21/2003	16:25	0	1/21/2003	17:07	-0.1
1/21/2003	16:26	-0.1	1/21/2003	17:08	0
1/21/2003	16:27	0.3	1/21/2003	17:09	0.1
1/21/2003	16:28	0	1/21/2003	17:10	0.2
1/21/2003	16:29	0.2	1/21/2003	17:11	0.2
1/21/2003	16:30	-0.1	1/21/2003	17:12	0.1
1/21/2003	16:31	-0.1	1/21/2003	17:13	0.1
1/21/2003	16:32	-0.1	1/21/2003	17:14	0.1
1/21/2003	16:33	0.3	1/21/2003	17:15	0.1
1/21/2003	16:34	0	1/21/2003	17:16	0.1
1/21/2003	16:35.	-0.3	1/21/2003	17:17	0.2
1/21/2003	16:36	-0.3	1/21/2003	17:18	0.1
1/21/2003	16:37	-0.4	1/21/2003	17:19	0.2
1/21/2003	16:38	-0.3	1/21/2003	17:20	0.1
1/21/2003	16:39	-0.3	1/21/2003	17:21	0.7
1/21/2003	16:40	-0.4	1/21/2003	17:22	0.6
1/21/2003	16:41	-0.3	1/21/2003	17:23	0.2
1/21/2003	16:42	-0.1	1/21/2003	17:24	0
1/21/2003	16:43	-0.3	Final Average*	·····	0.2
1/21/2003	16:44	-0.3	Maximum*		4
1/21/2003	16:45	-0.2	Minimum*		-0.4
1/21/2003	16:46	-0.1			
1/21/2003	16:47	-0.2	*Does not include I	nvalid Averag	ging Periods ("
1/21/2003	16:48	-0.3			. `
1/21/2003	16:49	-0.1			
1/21/2003	16:50	0			
1/21/2003	16:51	-0.2			
1/21/2003	16:52	0			
1/21/2003	16:53	0			
1/21/2003	16:54	0			
		-	4		

Company: Okeelanta CoGen

Period Start: 02/13/02

10:16

Plant:

lant.

Period End:

02/13/02

11:19

City/St:

South Bay, FL

Validation Type:

1/1 min

Source:

2/13/2002

2/13/2002

10:56

10:57

6.8

5.8

Stack 1

Averaging Period:

1 min

		verage			Average
	O	pacity_1		U	pacity_1
Period Start		<u>%</u>	Period Start		%
2/13/2002	10:16	4.6	2/13/2002	10:58	5.9
2/13/2002	10:17	4.5	2/13/2002	10:59	5.7
2/13/2002	10:18	5.1	2/13/2002	11:00	6.2
2/13/2002	10:19	4.8	2/13/2002	11:01	5.3
2/13/2002	10:20	5.5	2/13/2002	11:02	5.5
2/13/2002	10:21	6.7	2/13/2002	11:03	5,4
2/13/2002	10:22	5.1	2/13/2002	11:04	5.9
2/13/2002	10:23	4.2	2/13/2002	11:05	6
2/13/2002	10:24	4.5	2/13/2002	11:06	5.7
2/13/2002	10:25	4.4	2/13/2002	11:07	6.2
2/13/2002	10:26	4.4	2/13/2002	11:08	6.4
2/13/2002	10:27	5.4	2/13/2002	11:09	6
2/13/2002	10:28	5	2/13/2002	11:10	5.1
2/13/2002	10:29	5.4	2/13/2002	11:11	5.5
2/13/2002	10:30	4.9	2/13/2002	11:12	7.2
2/13/2002	10:31	5.2	2/13/2002	11:13	6.3
2/13/2002	10:32	4.9	2/13/2002	11:14	6
2/13/2002	10:33	5.4	2/13/2002	11:15	4.9
2/13/2002	10:34	5.5	2/13/2002	11:16	5.3
2/13/2002	10:35	5.3	2/13/2002	11:17	5.5
2/13/2002	10:36	4.6	2/13/2002	11:18	5.2
2/13/2002	10:37	4.8	2/13/2002	13:20	2.4
2/13/2002	10:38	5.5	Final Average*		5.5
2/13/2002	10:39	4.5	Maximum*		22.4
2/13/2002	10:40	4.5	Minimum*		4.2
2/13/2002	10:41	4.9	17413144444		1.2
2/13/2002	10:42	4.5	*Does not include I	nvalid Aver	aging Period
2/13/2002	10:42	4.3	Boes not metade i	iivand Aver	ignig i crioc
2/13/2002	10:43	4.5			
2/13/2002	10:45	4.6			
2/13/2002	10:45	4.8			
2/13/2002	10:40	6			
2/13/2002	10:48	4.8			
2/13/2002	10:49	4.9			
2/13/2002	10:49	4.9			
2/13/2002	10.50	4.6			
2/13/2002	10.51	4.0 5			
2/13/2002	10:52	4.7			
					<i>-</i> .
2/13/2002	10:54	5.6			,
2/13/2002	10:55	22.4			

Company: Okeelanta CoGen

Period Start: 02/13/02

12:09

Plant:

Period End:

02/13/02 13:13

City/St:

South Bay, FL

Validation Type:

1/1 min

Source:

2/13/2002

2/13/2002

12:49

12:50

4.1

3.9

Stack 1

Averaging Period:

1 min

Type:

e: Block Avg

		Average			Average
•		Opacity_1		(Opacity 1
Period Start		%	Period Start		%
2/13/2002	12:09	4	2/13/2002	12:51	6
2/13/2002	12:10	3.9	2/13/2002	12:52	4.3
2/13/2002	12:11	4.4	2/13/2002	12:53	4.9
2/13/2002	12:12	3.6	2/13/2002	12:54	4.6
2/13/2002	12:13	3.7	2/13/2002	12:55	5.4
2/13/2002	12:14	3.5	2/13/2002	12:56	4.4
2/13/2002	12:15	3.5	2/13/2002	12:57	4.1
2/13/2002	12:16	3.5	2/13/2002	12:58	4
2/13/2002	12:17	3.6	2/13/2002	12:59	4.5
2/13/2002	12:18	3.7	2/13/2002	13:00	4
2/13/2002	12:19	3.7	2/13/2002	13:01	4.2
2/13/2002	12:20	3.9	2/13/2002	13:02	4
2/13/2002	12:21	4.3	2/13/2002	13:03	4.1
2/13/2002	12:22	3.7	2/13/2002	13:04	4
2/13/2002	12:23	3.7	2/13/2002	13:05	32.6
2/13/2002	12:24	3.8	2/13/2002	13:06	13.9
2/13/2002	12:25	3.7	2/13/2002	13:07	5.9
2/13/2002	12:26	3.9	2/13/2002	13:08	5.6
2/13/2002	12:27	3.8	2/13/2002	13:09	4.9
2/13/2002	12:28	3.8	2/13/2002	13:10	5
2/13/2002	12:29	3.7	2/13/2002	13:11	4.6
2/13/2002	12:30	3.6	2/13/2002	13:12	4.9
2/13/2002	12:31	3.7	2/13/2002	13:13	4.5
2/13/2002	12:32	4.1	Final Average*		4.7
2/13/2002	12:33	5.1	Maximum*		32.6
2/13/2002	12:34	3.9	Minimum*	-	3.5
2/13/2002	12:35	3.8			
. 2/13/2002	12:36	3.7	*Does not include l	Invalid Aver	aging Periods ("N/A"
2/13/2002	12:37	3.7		•	
2/13/2002	12:38	3.8			
2/13/2002	12:39	3.9	•		
2/13/2002	12:40	3.7			
2/13/2002	12:41	3.7	•		
2/13/2002	12:42	3.6			
2/13/2002	12:43	3.8			
2/13/2002	12:44	3.9			
2/13/2002	12:45	3.6			
2/13/2002	12:46	3.6			
2/13/2002	12:47	3.8			
2/13/2002	12:48	4.1			_
2/12/2002	10.40	4 1			

Company: Okeelanta CoGen Period Start: 02/13/02

13:44

Plant:

Period End: 02/13/02 14:48

City/St:

South Bay, FL

Validation Type: 1 min

1/1 min

Source: Stack 1 Averaging Period:

		Average			Average
	O	pacity_1	•	C	pacity_1
Period Start		%	Period Start		%
2/13/2002	13:44	3.9	2/13/2002	14:26	3.8
2/13/2002	13:45	4	2/13/2002	14:27	4.4
2/13/2002	13:46	3.9	2/13/2002	14:28	4
2/13/2002	13:47	4.2	2/13/2002	14:29	4
2/13/2002	13:48	3.8	2/13/2002	14:30	3.9
2/13/2002	13:49	3.7	2/13/2002	14:31	4.1
2/13/2002	13:50	3.6	2/13/2002	14:32	4
2/13/2002	13:51	3.5	2/13/2002	14:33	4
2/13/2002	13:52	3.8	2/13/2002	14:34	4.5
2/13/2002	13:53	3.6	2/13/2002	14:35	4.4
2/13/2002	13:54	3.8	2/13/2002	14:36	3.9
2/13/2002	13:55	3.9	2/13/2002	14:37	4.1
2/13/2002	13:56	3.7	2/13/2002	14:38	4.1
2/13/2002	13:57	4.4	2/13/2002	14:39	3.9
2/13/2002	13:58	3.6	2/13/2002	14:40	3.9
2/13/2002	13:59	3.5	2/13/2002	14:41	3.8
2/13/2002	14:00	3.4	2/13/2002	14:42	3.9
2/13/2002	14:01	3.5	2/13/2002	14:43	3.6
2/13/2002	14:02	3.6	2/13/2002	14:44	3.7
2/13/2002	14:03	3.5	2/13/2002	14:45	3.9
2/13/2002	14:04	3.5	2/13/2002	14:46	3.9
2/13/2002	14:05	3.7	2/13/2002	14:47	3.7
2/13/2002	14:06	3.9	2/13/2002	14:48	3.7
2/13/2002	14:07	4	Final Average*		4.2
2/13/2002	14:08	3.6	Maximum*		22.3
2/13/2002	14:09	3.5	Minimum*		3.4
2/13/2002	14:10	3.4			3.4
2/13/2002	14:11	3.5	*Does not include l	nvalid Aver	aging Periods ("
2/13/2002	14:12	3.5	Does not metade i	iiivana 71vor	iging ronous (
2/13/2002	14:13	3.6		·	
2/13/2002	14:14	3.6			
2/13/2002	14:15	3.5			
2/13/2002	14:16	22.3			
2/13/2002	14:17	7.8	·		
2/13/2002	14:18	5.2			
2/13/2002	14:19	4.5			
2/13/2002	14:19	4.3			
2/13/2002	14:21	4.1		-	
2/13/2002	14:21	4.1			
2/13/2002	14:22	4.3			
2/13/2002	14:23	4.3	•		
2/13/2002	14:25	4		i	•

Company: Okeelanta CoGen Period Start: 02/14/02 09:35

Plant:

Period End:

02/14/02

City/St:

South Bay, FL

Validation Type:

10:39 1/1 min

Source:

2/14/2002

10:16

4.8

Stack 2

Averaging Period:

1 min

		verage	•		verage
	Op	oacity_1		OI	pacity_1
Period Start		%	Period Start		%
2/14/2002	9:35	4.8	2/14/2002	10:17	4.8
2/14/2002	9:36	5	2/14/2002	10:18	5
2/14/2002	9:37	4.6	2/14/2002	10:19	5.5
2/14/2002	9:38	5.2	2/14/2002	10:20	5
2/14/2002	9:39	4.8	2/14/2002	10:21	5.1
2/14/2002	9:40	4.7	2/14/2002	10:22	5.3
2/14/2002	9:41	5.1	2/14/2002	10:23	4.7
2/14/2002	9:42	4.7	2/14/2002	10:24	5.6
2/14/2002	9:43	4.6	2/14/2002	10:25	5.3
2/14/2002	9:44	4.5	2/14/2002	10:26	4.8
2/14/2002	9:45	4.7	2/14/2002	10:27	5.1
2/14/2002	9:46	4.8	2/14/2002	10:28	5.1
2/14/2002	9:47	4.8	2/14/2002	10:29	5.1
2/14/2002	9:48	4.8	2/14/2002	10:30	5.1
2/14/2002	9:49	4.8	2/14/2002	10:31	5.4
2/14/2002	9:50	5	2/14/2002	10:32	5.3
2/14/2002	9:51	5.5	2/14/2002	10:33	5.4
2/14/2002	9:52	5.2	2/14/2002	10:34	5.3
2/14/2002	9:53	4.9	2/14/2002	10:35	4.8
2/14/2002	9:54	5.1	2/14/2002	10:36	5.5
2/14/2002	9:55	5.4	2/14/2002	10:37	5.4
2/14/2002	9:56	6.3	2/14/2002	10:38	5.4
2/14/2002	9:57	5.7	2/14/2002	10:39	3.7
2/14/2002	9:58	5.3	Final Average*		5.1
2/14/2002	9:59	5	Maximum*		6.3
2/14/2002	10:00	4.7	Minimum*		4.5
2/14/2002	10:01	5.1			4.5
2/14/2002	10:02	5.1	*Does not include l	nvalid Averag	ging Periods ("N/A
2/14/2002	10:03	4.8	Does not metade i	iivaila rivelag	sing renous (14/2
2/14/2002	10:04	5.4			
2/14/2002	10:05	5			
2/14/2002	10:06	5.2	•		
2/14/2002	10:07	5.7			
2/14/2002	10:08	5.2			
2/14/2002	10:09	5.3			
2/14/2002	10:10	5.2			
2/14/2002	10:10	5.4			
2/14/2002	10:11	6.1			
2/14/2002	10:12	5.1			
2/14/2002	10:13	5.1			
2/14/2002	10:14	4.7			
2/14/2002	10.15	4.7			

Company: Okeelanta CoGen Period Start: 02/14/02 11:10

Plant:

Period End:

02/14/02 1/1 min

City/St: South Bay, FL

Validation Type: Averaging Period: 1 min

12:15

Source: Stack 2

	A	verage		A	verage	
	O	pacity 1		Opacity_1		
Period Start	•	%	Period Start		%	
2/14/2002	11:10	4.5	2/14/2002	11:52	4	
2/14/2002	11:11	4.3	2/14/2002	11:53	3.9	
2/14/2002	11:12	4.1	2/14/2002	11:54	4.1	
2/14/2002	11:13	4.3	2/14/2002	11:55	4.1	
2/14/2002	11:14	4.1	2/14/2002	11:56	4.1	
2/14/2002	11:15	5.4	2/14/2002	11:57	4	
2/14/2002	11:16	4.2	2/14/2002	11:58	3.9	
2/14/2002	11:17	4.3	2/14/2002	11:59	4.1	
2/14/2002	11:18	4.2	2/14/2002	12:00	4.2	
2/14/2002	11:19	4.3	2/14/2002	12:01	4.5	
2/14/2002	11:20	4	2/14/2002	12:02	4.1	
2/14/2002	11:21	4.2	2/14/2002	12:03	4	
2/14/2002	11:22	4	2/14/2002	12:04	3.9	
2/14/2002	11:23	3.9	2/14/2002	12:05	4	
2/14/2002	11:24	3.8	2/14/2002	12:06	4.2	
2/14/2002	11:25	4.1	2/14/2002	12:07	4.4	
2/14/2002	11:26	4.7	2/14/2002	12:08	4.2	
2/14/2002	11:27	4.3	2/14/2002	12:09	4.1	
2/14/2002	11:28	3.9	2/14/2002	12:10	4.4	
2/14/2002	11:29	4	2/14/2002	12:11	4	
2/14/2002	11:30	4.2	2/14/2002	12:12	4	
2/14/2002	11:31	4.2	2/14/2002	12:13	4.2	
2/14/2002	11:32	4.1	2/14/2002	12:14	4.3	
2/14/2002	11:33	4.3	2/14/2002	12:15	4.3	
2/14/2002	11:34	4	Final Average*		4.3	
2/14/2002	11:35	4	Maximum*		9.9	
2/14/2002	11:36	4	Minimum*		3.8	
2/14/2002	11:37	4.2				
2/14/2002	11:38	4.5	*Does not include 1	nvalid Avera	ging Periods ("N/A")	
2/14/2002	11:39	4.1				
2/14/2002	11:40	4.2				
2/14/2002	11:41	6.7				
2/14/2002	11:42	4.3				
2/14/2002	11:43	9.9				
2/14/2002	11:44	4.7				
2/14/2002	11:45	4.1				
2/14/2002	11:46	4.1				
2/14/2002	11:47	4				
2/14/2002	11:48	4.1				
2/14/2002	11:49	4.1				
2/14/2002	11:50	3.9				
2/14/2002	11:51	3.9				

Company: Okeelanta CoGen

Period Start: 02/14/02

12:49

Plant:

lant:

Period End:

02/14/02 13:54

City/St:

South Bay, FL

Validation Type:

1/1 min

Source:

2/14/2002

2/14/2002

2/14/2002

2/14/2002

2/14/2002

2/14/2002

2/14/2002

2/14/2002

13:23

13:24

13:25

13:26

13:27

13:28

13:29

13:30

3.6

3.6

3.5

3.6

3.6 3.7

3.7

3.9

Stack 2

Averaging Period:

1 min

Period Start	Average Opacity_1 %		Period Start	Average Opacity_1 %		
2/14/2002	12:49	4.1	2/14/2002	13:31	4	
2/14/2002	12:50	4.1	2/14/2002	13:32	3.8	
2/14/2002	12:51	4	2/14/2002	13:33	3.5	
2/14/2002	12:52	4.2	2/14/2002	13:34	4.1	
2/14/2002	12:53	4.9	2/14/2002	13:35	4.1	
2/14/2002	12:54	4.2	2/14/2002	13:36	5.2	
2/14/2002	12:55	4	2/14/2002	13:37	4.8	
2/14/2002	12:56	4.1	2/14/2002	13:38	3.9	
2/14/2002	12:57	4	2/14/2002	13:39	3.8	
2/14/2002	12:58	4.1	2/14/2002	13:40	3.9	
2/14/2002	12:59	4	2/14/2002	13:41	4	
2/14/2002	13:00	3.9	2/14/2002	13:42	3.8	
2/14/2002	13:01	3.8	2/14/2002	13:43	4.1	
2/14/2002	13:02	3.6	2/14/2002	13:44	3.7	
2/14/2002	13:03	3.6	2/14/2002	13:45	3.7	
2/14/2002	13:04	3.6	2/14/2002	13:46	3.7	
2/14/2002	13:05	3.8	2/14/2002	13:47	3.6	
2/14/2002	13:06	3.9	2/14/2002	13:48	3.8	
2/14/2002	13:07	3.7	2/14/2002	13:49	3.5	
2/14/2002	13:08	3.6	2/14/2002	13:50	3.5	
2/14/2002	13:09	3.7	2/14/2002	13:51	3.6	
2/14/2002	13:10	3.8	2/14/2002	13:52	3.7	
2/14/2002	13:11	3.8	2/14/2002	13:53	3.7	
2/14/2002	13:12	3.6	2/14/2002	13:54	4.3	
2/14/2002	13:13	3.5	Final Average*		3.8	
2/14/2002	13:14	3.5	Maximum*		5.2	
2/14/2002	13:15	3.6	Minimum*		3.5	
2/14/2002	13:16	3.6				
2/14/2002	13:17	3.6	*Does not include I	nvalid Avera	iging Periods ("N/A"	
2/14/2002	13:18	3.9			•	
2/14/2002	13:19	3.8				
2/14/2002	13:20	3.6				
2/14/2002	13:21	3.7				
2/14/2002	13:22	3.7				

Company: Okeelanta CoGen

Period Start: 02/12/02

10:14 11:19

Plant: City/St:

2/12/2002

10:55

4.8

South Bay, FL

Period End: Validation Type:

02/12/02 1/1 min

Source: Stack 3

Averaging Period:

1 min

Type:

pe: Block Avg

		verage		Average		
	Opacity_1			Opacity_1		
Period Start		%	Period Start		%	
2/12/2002	10:14	3.7	2/12/2002	10:56	4.8	
2/12/2002	10:15	3.8	2/12/2002	10:57	4.6	
2/12/2002	10:16	3.9	2/12/2002	10:58	4.4	
2/12/2002	10:17	3.8	2/12/2002	10:59	4.4	
2/12/2002	10:18	3.6	2/12/2002	11:00	4.4	
2/12/2002	10:19	3.6	2/12/2002	11:01	4.5	
2/12/2002	10:20	3.6	2/12/2002	11:02	4.2	
. 2/12/2002	10:21	3.6	2/12/2002	11:03	4.1	
2/12/2002	10:22	3.5	2/12/2002	11:04	3.9	
2/12/2002	10:23	3.6	2/12/2002	11:05	4.2	
2/12/2002	10:24	3.6	2/12/2002	11:06	4	
2/12/2002	10:25	3.6	2/12/2002	11:07	4	
2/12/2002	10:26	3.7	2/12/2002	11:08	4	
2/12/2002	10:27	3.6	2/12/2002	11:09	4.1	
2/12/2002	10:28	3.6	2/12/2002	11:10	3.9	
2/12/2002	10:29	3.8	2/12/2002	11:11	3.9	
2/12/2002	10:30	3.6	2/12/2002	11:12	3.9	
2/12/2002	10:31	3.7	2/12/2002	11:13	3.8	
2/12/2002	10:32	3.8	2/12/2002	11:14	4.2	
2/12/2002	10:33	4	2/12/2002	11:15	4	
2/12/2002	10:34	3.7	2/12/2002	11:16	3.9	
2/12/2002	10:35	6.5	2/12/2002	11:17	. 3.8	
2/12/2002	10:36	4.5	2/12/2002	11:18	4	
2/12/2002	10:37	4.2	2/12/2002	11:19	3.9	
2/12/2002	10:38	4	Final Average*		5.1	
2/12/2002	10:39	4.2	Maximum*		45.5	
2/12/2002	10:40	4.2	Minimum*		3.5	
2/12/2002	10:41	45.5				
2/12/2002	10:42	14.1	*Does not include I	nvalid Aver	aging Periods ("N	√A")
2/12/2002	10:43	9.7			,	,
2/12/2002	10:44	7.6				
2/12/2002	10:45	6.7				
2/12/2002	10:46	6.5				
2/12/2002	10:47	5.7				
2/12/2002	10:48	5.6				
2/12/2002	10:49	5.3				
2/12/2002	10:50	5				
2/12/2002	10:51	5				
2/12/2002	10:52	5.1				
2/12/2002	10:53	4.7				
2/12/2002	10:54	4.5				

Company: Okeelanta CoGen Period Start: 02/12/02 12:35

Plant:

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

13:05

13:06

13:07

13:08

13:09

13:10

13:11

13:12

13:13

13:14

13:15

13:16

Period End:

City/St:

South Bay, FL

Validation Type: 1/1 min 13:39

Source: Stack 3 Averaging Period:

1 min

02/12/02

Block Avg Type:

		Average Opacity_1			Average Opacity_1
Period Start		%	Period Start		%
2/12/2002	12:35	3	2/12/2002	13:17	3.4
. 2/12/2002	12:36	2.9	2/12/2002	13:18	3.3
2/12/2002	12:37	3	2/12/2002	13:19	3.2
2/12/2002	12:38	3	2/12/2002	13:20	3.3
2/12/2002	12:39	3.1	2/12/2002	13:21	3.1
2/12/2002	12:40	3	2/12/2002	13:22	3
2/12/2002	12:41	3	2/12/2002	13:23	3.4
2/12/2002	12:42	2.9	2/12/2002	13:24	3.2
2/12/2002	12:43	2.9	2/12/2002	13:25	3.1
2/12/2002	12:44	2.8	2/12/2002	13:26	3
2/12/2002	12:45	2.7	2/12/2002	13:27	. 3.2
2/12/2002	12:46	3	. 2/12/2002	13:28	3.1
2/12/2002	12:47	2.9	2/12/2002	13:29	3.1
2/12/2002	12:48	. 3	2/12/2002	13:30	. 3.1
2/12/2002	12:49	3.1	2/12/2002	13:31	3
2/12/2002	12:50	3.1	2/12/2002	13:32	3.2
2/12/2002	12:51	3.1	2/12/2002	13:33	3
2/12/2002	12:52	3	2/12/2002	13:34	3.3
2/12/2002	12:53	3	2/12/2002	13:35	3.3
2/12/2002	12:54	2.9	2/12/2002	13:36	3.2
2/12/2002	12:55	3.1	2/12/2002	13:37	3.1
2/12/2002	12:56	3	2/12/2002	13:38	3.2
2/12/2002	12:57	3.1	2/12/2002	13:39	3:3
2/12/2002	12:58	3	Final Average*		3.1
2/12/2002	12:59	3	Maximum*		3.5
2/12/2002	13:00	3.1	Minimum*		2.7
2/12/2002	13:01	3.2			
2/12/2002	13:02	3	*Does not include I	nvalid Av	eraging Periods
2/12/2002	13:03	3			
2/12/2002	13:04	3			

2.9

3.4

3.5

3.3

3.3

3.5

3.3

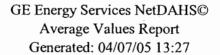
3.3

3.4

3.3

3.4

s ("N/A")



Company: Okeelanta CoGen Period Start: 02/12/02 14:11

02/12/02

Plant:

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

2/12/2002

14:39

14:40

14:41

14:42

14:43

14:44

14:45

14:46

14:47

14:48

14:49

14:50

14:51

14:52

Period End:

15:15

City/St: South Bay, FL

Validation Type: Averaging Period:

1/1 min

Source: Stack 3

1 min Type: Block Avg

		verage pacity_1			Average Opacity_1
Period Start	_	<u>%</u>	Period Start	<u> </u>	%
2/12/2002	14:11	3.1	2/12/2002	14:53	3.7
2/12/2002	14:12	2.8	2/12/2002	14:54	· 3.8
2/12/2002	14:13	3	2/12/2002	14:55	3.8
2/12/2002	14:14	2.8	2/12/2002	14:56	3.7
2/12/2002	14:15	2.8	2/12/2002	14:57	4
2/12/2002	14:16	2.8	2/12/2002	14:58	3.6
2/12/2002	14:17	2.8	2/12/2002	14:59	3.6
2/12/2002	14:18	2.9	2/12/2002	15:00	. 3.7
2/12/2002	14:19	2.9	2/12/2002	15:01	3.9
2/12/2002	14:20	2.9	2/12/2002	15:02	3.9
2/12/2002	14:21	3	2/12/2002	15:03	3.8
2/12/2002	14:22	2.7	2/12/2002	15:04	3.6
2/12/2002	14:23	2.8	2/12/2002	15:05	3.8
2/12/2002	14:24	2.8	2/12/2002	15:06	4.3
2/12/2002	14:25	3.1	2/12/2002	15:07	4
2/12/2002	14:26	3	2/12/2002	15:08	4.1
2/12/2002	14:27	3.1	2/12/2002	15:09	4.2
2/12/2002	14:28	3.1	2/12/2002	15:10	4
2/12/2002	14:29	2.9	2/12/2002	15:11	3.9
2/12/2002	14:30	2.8	2/12/2002	15:12	4.1
2/12/2002	14:31	3	. 2/12/2002	15:13	4.3
2/12/2002	14:32	2.8	2/12/2002	15:14	4.2
2/12/2002	14:33	3.1	2/12/2002	15:15	4.2
2/12/2002	14:34	3.2	Final Average*		3.4
2/12/2002	14:35	3.3	Maximum*		4.3
2/12/2002	14:36	. 3	Minimum*		2.7
2/12/2002	14:37	3.1			
2/12/2002	14:38	3.4	*Does not include l	nvalid Av	eraging Period

3.5

3.3

3.3

3.1

3.5

3.2

3.4

3.5

3.7

3.2

3.5

3.7

3.6

^{*}Does not include Invalid Averaging Periods ("N/A")