Memorandum

Florida Department of Environmental Protection

TO:

Clair Fancy, Chief, BAR

THROUGH:

Al Linero, Administrator - New Source Review Section (20)

FROM:

Jeff Koerner, New Source Review Section

DATE:

May 24, 2001

SUBJECT:

Project No. 0990005-009-AC

Draft Air Permit No. PSD-FL-169A

Okeelanta Corporation, Sugar Mill and Refinery Conversion of Boiler No. 16 to Natural Gas

Attached for your review are the following items:

Intent to Issue Permit and Public Notice Package;

- Technical Evaluation and Preliminary Determination;
- Draft Permit; and
- PE Certification

The Technical Evaluation and Preliminary Determination provides a detailed description of the project, the rule applicability, and the BACT determinations. The P.E. certification briefly summarizes proposed project and BACT determinations. Day #74 is June 4, 2001. I recommend your approval of the attached Draft Permit for this project.

CHF/AAL/ifk

Attachments

Florida Department of Environmental Protection
Division of Air Resources Management
Bureau of Air Regulation
New Source Review Section
2600 Blair Stone Road, MS #5505
Tallahassee, Florida, 32399-2400

P.E. CERTIFICATION STATEMENT

PERMITTEE

Okeelanta Corporation 21250 U.S. Highway 27 South Bay, FL 33493 Project No. 0990005-009-AC Draft Permit No. PSD-FL-169A Facility 1D No. 0990005 SIC Nos. 2061, 2062, and 4911

PROJECT DESCRIPTION

The applicant, Okeelanta Corporation, operates an existing sugar mill and sugar refinery located approximately six miles south of South Bay on U.S. 27 in Palm Beach County, Florida. Adjacent to the sugar mill and refinery is Okeelanta Power L.P.'s existing cogeneration plant, which fires biomass to produce steam for the mill and generate electricity for sale to the power grid. The applicant proposes to modify the burner system of existing mill Boiler No. 16 to accommodate natural gas as the primary fuel and very low sulfur distillate oil as an alternate fuel. This unit is a package steam boiler with a capacity of 150,000 pounds per hour of steam with a heat input of approximately 200 mmBTU per hour. The existing boiler was subject to PSD during initial construction and has a NOx CEMS and opacity COMS in accordance with the NSPS Subpart Db requirements for boilers.

The existing facility is a PSD-major source of air pollution located in an area that is in attainment (or designated as unclassifiable) for all air pollutants subject to a National Ambient Air Quality Standard (NAAQS). As such, BACT determinations are required for NOx and PM10 because emissions from the boiler exceed the PSD Significant Emission Rates for these pollutants. In addition, BACT determinations are required for emissions of PM and SO2 in accordance with Rule 62-296.406, F.A.C. (small boiler BACT). I recommend the following emissions standards as BACT for this project:

Pollutant	BACT Standards	BACT Controls
СО	CO (gas) ≤ 0.10 lb/mmBTU based on a 3-hour test average CO (oil) ≤ 0.11 lb/mmBTU based on a 3-hour test average	Efficient combustion of clean fuels (Avoids BACT determination.)
NOx	NOx (gas) \leq 0.06 lb/mmBTU based on a 24-hour (daily) CEMS average NOx (oil) \leq 0.12 lb/mmBTU based on a 24-hour (daily) CEMS average	Low NOx burners with flue gas recirculation (≈ 15%)
PM	Opacity (gas and oil) ≤ 10% based on a 6-minute COMS average, except for one 6-minute period per hour not to exceed 20% opacity	Efficient combustion of clean fuels
	PM (oil) ≤ 0.03 lb/mmBTU based on initial 3-hour test average	
SO ₂	Efficient combustion of pipeline-quality natural gas and very low sulfur distillate oil (< 0.05% sulfur by weight)	Very low sulfur fuels

Our staff meteorologist reviewed the applicant's Air Quality Analysis and determined that the project would not result in any significant impacts. Therefore, the Department has reasonable assurance that the proposed project, as described in the application and subject to the conditions of the Draft Permit, will not cause or significantly contribute to a violation of any AAQS or PSD increment.

I HEREBY CERTIFY that the air pollution control engineering features described in the above referenced application and subject to the proposed permit conditions provide reasonable assurance of compliance with applicable provisions of Chapter 403, Florida Statutes, and Florida Administrative Code Chapters 62-4 and 62-204 through 62-297. However, I have not evaluated and I do not certify aspects of the proposal outside of my area of expertise (including but not limited to the electrical, mechanical, structural, hydrological, and geological features).

Jeffery F. Koerner, P.E.

Registration Number: 49441

Jeffeny J. Koun

5-24-01

(Date)

Golder Associates Inc.

6241 NW 23rd Street, Suite 500 Gainesville, FL 32653-1500 Telephone (352) 336-5600 Fax (352) 336-6603



May 31, 2001

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Florida Department of Environmental Protection Bureau of Air Regulation, New Source Review Section 2600 Blair Stone Road, MS 5500 Tallahassee, Florida 32399-2400 RECEIVED

JUN 0 1 2001

BUREAU OF AIR REGULATION

Attention: Mr. A. A. Linero, P.E.

RE: OKEELANTA CORPORATION (ID NO. 0990005)

OKEELANTA SUGAR AND REFINERY MILL

BOILER NO. 16 PSD APPLICATION

Dear Mr. Linero:

Okeelanta Corporation submitted a prevention of significant deterioration (PSD) application to Florida Department of Environmental Protection (FDEP) to modify Boiler No. 16 at their sugar and refinery mill in March 2000. This application was submitted to obtain a construction permit to convert Boiler No. 16 into a dual fuel-fired boiler and to increase operating hours. Emission increases mandated PSD review for particulate matter (PM_{10}) , nitrogen oxides (NO_x) , and carbon monoxide (CO).

Upon further investigation and collaboration with the vendor of the new dual fuel-fired burner, it has been determined that the burner will be able to achieve lower CO emissions than what was reported in the PSD application. In the application, the maximum CO emissions were stated as 0.16 lb/MMBtu due to fuel oil firing and 0.15 lb/MMBtu due to natural gas firing, based on vendor guarantees. These emission rates resulted in a maximum annual emission rate of 140.90 tons per year.

It has now been determined that maximum CO emissions will not exceed 0.11 lb/MMBtu due to fuel oil firing and 0.10 lb/MMBtu due to natural gas firing. These lower limits are based in large part on previous CO testing performed on Boiler No. 16 while burning fuel oil, which demonstrated emissions lower than 0.10 lb/MMBtu. The new emission factors will lower the maximum annual CO emission rate for Boiler No. 16 to 96.19 tons per year.

Okeelanta would like to update the PSD application to reflect the latest emission rates for the boiler. One page from the application form and four tables from the PSD report are affected by this change. These pages have been revised and are attached for your consideration. The increase in CO emissions will no longer exceed the PSD significant rate and no longer require PSD review. Okeelanta asks that the modeling analysis and the BACT review for CO presented in the original application be set aside, since they are no longer required.

Please call or write if any questions about this change.

Sincerely,

GOLDER ASSOCIATES INC.

David A. Buff, P.E., Q.E.P.

David a Buff

Principal Engineer

Florida P. E. #19011

SEAL

DB/jkw

Enclosures

cc:

M. Capone

J. Meriwether

S. Watson

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C. Holladay S. Galdmorn, SED D. Graziane, PBCHD

NPS

Emissions Unit Information Section	1	of .	1	Mill Boiler No. 16
Pollutant Detail Information Page	5	of	10	Carbon Monoxide- CO

G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units -

Emissions-Limited and Preconstruction Review Pollutants Only)

Potential/Fugitive Emissions

1.	Pollutant Emitted:	2.	Total	l Percer	nt Efficie	ncy c	of Control:		
	со								
3.	Potential Emissions:					4.	Synthetica	lly	
	22.22 lb/hour	96	19	tons/y	year]	Limited?	[
5.	Range of Estimated Fugitive Emissions:			to	t	ons/y	ear		
6.	Emission Factor: 0.11 lb/MMBtu						Emissions		
-							Method Co	ode:	
	Reference: Manufacturer's Estimate						_		
0	Calculation of Projectors (Books to 600 above to						2		\dashv
8.	Calculation of Emissions (limit to 600 charact	ters)							
	See Table 2-1 for calculations								
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9	Pollutant Potential/Fugitive Emissions Comm	neni	(lim	it to 20	0 charac	ters):		 -	
	Tomatan Total May 1 agrave Emilione Comm		(,.			
	Emission factor based on fuel oil-firing.								
	<u></u>								
<u>A1</u>	lowable Emissions Allowable Emissions		of_						
1.	Basis for Allowable Emissions Code:	2.	Futi	ure Effe	ective Da	ate of	Allowable	<u>;</u>	
			Emi	ssions:					
3.	Requested Allowable Emissions and Units:	4.	Equ	ivalent	Allowal	ble Er	nissions:		
				lb	/hour		tons/y	ear	
5.	Method of Compliance (limit to 60 characters	s):							
	• ,	-							
6	Allowable Emissions Comment (Desc. of Op	erati	no M	(lethod)	(limit to	200	characters'):	\dashv
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DEP Form No. 62-210.900(1) - Form Effective: 2/11/99

Table 1-1. Net Emissions Increase for Modification to Okeelanta Boiler No. 16 (revised 5/30)

Pollutant	Net Increase in	PSD Significant	PSD
1 Onutain	Emissions ^a	Rate	Review
	(TPY)	(TPY)	Applies?
Particulate Matter (PM)	22.16	25	No
Particulate Matter (PM ₁₀)	22.16	15	Yes
Sulfur Dioxide	39.38	40	No
Nitrogen Oxides	113.77	40	Yes
Carbon Monoxide	96.19	100	No
Volatile Organic Compounds	27.73	40	No
Sulfuric Acid Mist	1.75	7	No
Lead	6.23E-03	0.6	No
Mercury	2.09E-03	0.1	No
Beryllium	2.04E-03	4.00E-04	Yes
Fluorides		3	No

Since Boiler No. 16 has operated very little in the last several years, the current emissions from Boiler No. 16 were assumed to be zero.
 Thus, the net increase in emissions are equal to the future maximum emissions of Boiler No. 16.

Table 2-1. Future Maximum Emissions from Boiler No. 16, Okeelanta Corporation (revised 5/30/01)

		P	iatural	Gas Combustion				N	lo. 2 Fı	el Oil Combustio	on n		Annual Emissions	Maximum Annual
Regulated	Emission	Emission		Activity	Hourly	Annual	Emission	Emission		Activity	Hourly	Annual	With Maximum	Emissions Due
Pollutant	Factor	Factor	Ref.	Factor ^a	Emissions	Emissions ^b	Factor	Factor	Ref.	Factor*	Emissions	Emissions ^c	Fuel Oil Firing	to Any Combination
	(lb/10 ⁶ scf)	(lb/MMBtu)		(MMBtu/hr)	(lb/hr)	(TPY)	(lb/1000 gal)	(lb/MMBtu)		(MMBtu/hr)	(lb/hr)	(TPY)	(TPY)	(TPY)
Particulate Matter (PM)	1.9	1.86E-03	1	211	0.39	1.72		0.032	4	202	6.46	21.76	22.16	22.10
articulate Matter (PM ₁₀)	1.9	1.86E-03	1	211	0.39	1.72	**	0.032	4	202	6.46	21.76	22.16	22.10
Sulfur dioxide (SO ₂)	0.6	5.88E-04	1	211	0.12	0.54	7.85	0.058	5	202	11.66	39.25	39.38	39.3
Vitrogen oxides (NO _x)		0.055	2	211	11.61	50.83		0.15	2	202	30.30	102.00	113.77	113.7
Carbon monoxide (CO)		0.10	2	211	21.10	92.42		0.11	2	202	22.22	74.80	96.19	96.19
/oc		0.03	2	211	6.33	27.73		0.03	2	202	6.06	20.40	26.82	27.73
Sulfuric acid mist (SAM)		3.60E-05	3	211	7.60E-03	0.03		0.0026	6	202	0.52	1.75	1.75	1.7:
ead (Pb)	5.E-04	4.90E-07	- 1	211	1.03E-04	4.53E-04		9.00E-06	5	202	1.82E-03	6.12E-03	6.23E-03	6.23E-0
Aercury (Hg)	2.6E-04	2.55E-07	- 1	211	5.38E-05	2.36E-04		3.00E-06	5	202	6.06E-04	2.04E-03	2.09E-03	2.09E-0
leryllium (Be)	1.2E-05	1.18E-08	ı	211	2.49E-06	1.09E-05		3.00E-06	5	202	6.06E-04	2.04E-03	2.04E-03	2.04E-0
luorides (FI)														-

References:

- 1. Factors for natural gas combustion from AP-42, Tables 1.4-1, 1.4-2 and 1.4-4 (7/98). Factors were converted to lb/MMBtu by dividing by 1,020 Btu/scf.
- 2. Proposed emission limits. Based on emission guarantees from vendor.
- 3. Based on similar derivation of sulfuric acid mist from AP-42 for fuel oil. 5% of SO₂ becomes SO₃ then take into account the ratio of sulfuric acid mist and gaseous sulfate molecular weights (98/80).
- 4. Based on emission test results for Boiler No. 16.
- 5. Factors for No. 2 fuel oil combustion, AP-42 Table 1.3-1, 1.3-3, and 1.3-10 (9/98). A heating value of 136,000 Btu/gal and a maximum sulfur content of 0.05% were used for the No. 2 fuel oil.
- 6. The emission factor for SO₃ emissions from a No. 2 fuel fired boiler with low NOx burners (5.7S lb/10³ gal where S is the sulfur content) was multiplied by the ratio of sulfuric acid mist and gaseous sulfate molecular weights (98/80).

Footnotes

- * The proposed maximum permitted heat input rate is 211 MMBtu/hr for natural gas and 202 MMBtu/hr for fuel oil.
- b Based on maximum proposed operation of 8,760 hours.
- 6 Based on maximum proposed limit for 0.05% sulfur fuel oil of 10,000,000 gallons/yr, equivalent to 6,733 hours per year at 202 MMBtu/hr (1,360,000 MMBtu/yr).
- ⁴ Based on emissions due to maximum fuel oil usage (10,000,000 gal/yr or 1,360,000 MMBtu/yr) and the remaining due to natural gas (427,697 MMBtu/yr).
- 6 Maximum emissions predicted for either natural gas combustion only, No. 2 fuel oil combustion only, or a combination of No. 2 fuel oil and natural gas combustion.

Sample Calculations:

Hourly Emissions = Emission Factor x Activity Factor

Annual Emissions = Hourly Emissions x hours of operation (hrs/yr) / 2,000 (lb/ton)

Annual Emissions due to firing both fuels = Annual Emissions due to fuel oil + [(Hourly emissions due to natural gas x (8,760 hrs/yr - 6,733 hrs/yr)/ 2,000 (lb/ton)

Table 3-3. Net Emissions Increase for Modification to Okeelanta Boiler No. 16 (revised 5/30/01)

Pollutant	Net Increase in	PSD Significant	PSD
	Emissions ^a (TPY)	Rate (TPY)	Review Applies?
Particulate Matter (PM)	22.16	25	No
Particulate Matter (PM ₁₀)	22.16	15	Yes
Sulfur Dioxide	39.38	40	No
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Beryllium	2.04E-03	4.00E-04	Yes
Fluorides		3	No

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Table 5-6. Future Operating Parameters for Boiler No. 16, Okeelanta Corporation (revised 5/30/01)

Parameter	Value				
Stack Height	75 ft				
Stack Diameter	5 ft				
Gas Flow Rate	88,200 acf	m			
Velocity	75 ft/s				
Temperature	410 deg	g. F			
Regulated Pollutant	Hourly Emissions				
	(lb/hr)	(g/s)			
Particulate Matter (PM)	6.46	0.81			
Particulate Matter (PM ₁₀)	6.46	0.81			
Sulfur dioxide (SO ₂)	11.66	1.47			
Nitrogen oxides (NO _x)	30.30	3.82			
Carbon monoxide (CO)	22.22	2.80			
VOC	6.33	0.80			
Sulfuric acid mist (SAM)	0.52	0.07			
Lead (Pb)	1.82E-03	2.29E-04			
Mercury (Hg)	6.06E-04	7.64E-05			
Beryllium (Be)	6.06E-04	7.64E-05			
Fluorides (Fl)					