

OGDEN MARTIN SYSTEMS OF HILLSBOROUGH INC.

40 LANE ROAD
CN 2615
FAIRFIELD, NEW JERSEY 07007-2615
(201) 882-9000



AN OGDEN COMPANY

June 11, 1987

HC-0867L
C-1005

DER
JUN 15 1987
BAQM

Mr. Jerry Campbell
Hillsborough County Environmental Protection Commission
1900 9th Avenue
Tampa, FL 33605

Subject: Hillsborough County Florida
Solid Waste Energy Recovery Project
Supplemental Information for Retesting
Scheduled Week of June 15, 1987

Dear Mr. Campbell:

This notice is sent as a matter of clarification to my letter of June 10, 1987, advising you of our intent to utilize CARB 100 as the procedure for retesting for volatile hydrocarbons (VOC) at the Hillsborough County Solid Waste Energy Recovery Facility. The procedure referred to as CARB 100 is, in fact, EPA method 25A and is at present being utilized by EPA in testing currently in progress at Ogden Martin Systems Marion County Oregon Facility.

By separate cover, we have forwarded to your attention a full copy of the "Radian Source Test Plan" prepared for the EPA testing at Marion County. It is our intent to utilize EPA method 25A as stated in the provided Radian Test Plan for Marion County for the retesting for VOC's at the Hillsborough County Solid Waste Energy Recovery Project the week of June 15th, 1987.

As discussed with W. Schroeder (HCEPC) and Dave McNeil (EPA Region IV) by conference call on June 11, 1987, OMSH will test using EPA method 25A separate and simultaneous in both a wet and dry DIF configuration. OMSH understands that EPA Region IV recognizes the wet DIF configuration. We are conducting the dry configuration for comparison.

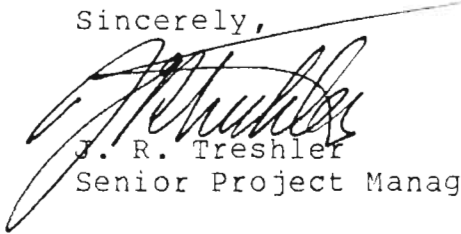
Mr. Jerry Campbell

-2 -

June 11, 1987

We hope this clarification will allow us to proceed with our plan for retesting. Please advise us of any further questions or comments directly associated with this issue.

Sincerely,



J. R. Treshler
Senior Project Manager

JRT:hn

cc: R. Hauser
P. Stoller
D. Strobridge
Daryl Smith
Tom Smith
D. Elias
D. Dee
D. Knight
W. Schroeder
Claire Fancy
Paul Reiner mann
D. McNeil

**OGDEN MARTIN SYSTEMS
OF HILLSBOROUGH INC.**

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CN 2615
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AN OGDEN COMPANY

DER

JUN 15 1987

BAQM

June 10, 1987

HC-0866L
C-1005

Mr. Jerry Campbell
Hillsborough County Environmental Protection Commission
1900 9th Avenue
Tampa, FL 33605

Subject: Hillsborough County Florida
Solid Waste Energy Recovery Project
Environmental Testing Report

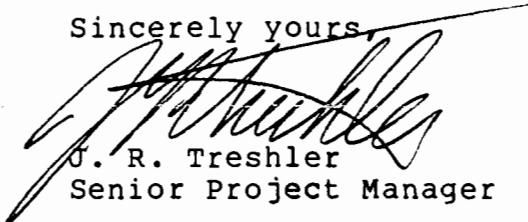
Dear Mr. Campbell:

Per the request of Bill Schroder, we are officially advising you of our intent to delay issuance of the Emissions Testing Report for the above stated project from the scheduled date of June 15 1987 until June 22, 1987.

As has been discussed with you, in our conversation of June 9, 1987, we have found certain irregularities in the results obtained for H₂SO₄ acid gas mist and VOC testing. We feel essential that we explain and document to you as part of our report submittal. We feel we will have our explanation prepared and ready for issuance to you by June 22, 1987.

We appreciate your cooperation on this issue.

Sincerely yours,


J. R. Treshler
Senior Project Manager

JRT:hn

cc: D. Strobbridge
P. Stoller
R. Hauser
T. Smith
D. Dee
D. Knight
Daryl Smith
A. Phillips
Ken Hernandez
W. Schroder
Paul Reinermann
Claire Fancy
Chi-Sun Lee

Hillsborough County — DER - 4/10/87

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Wm. A. GILLEN Jr.	"	813-273-5000
Joseph Freshner	Ogden Projects	201-882-9000
Richard Seelinger	" " " "	" " " "
Tom ROGERS	DER- BAQM	(904) 488-1344
Pradeep Raval	"	"
C H Fancy	"	"

BEST AVAILABLE COPY

2 Nov. 1987

Atlanta, GA

copy



UNITED STATES ENVIRONMENTAL PROTECTION AGENCY

REGION IV

345 COURTLAND STREET
ATLANTA, GEORGIA 30365

NOV 2 1987

4APT/APB-am

DER

NOV 4 1987

BAQM

Mr. C. H. Fancy, P.E., Chief
Bureau of Air Quality Management
Twin Towers Office Building
2600 Blair Stone Road
Tallahassee, Florida 32301-2400

Re: Hillsborough County PSD-FL-120

Dear Mr. Fancy:

This is to acknowledge receipt of your October 14, 1987, PSD final determination for modifications at the above referenced facility. We have reviewed the changes made to the draft permits submitted to EPA on July 14, 1987, and find them to be in accordance to our recommendations of September 11, 1987. We, therefore, concur on your final determination and the permits issued to Hillsborough County.

We will retain copies of the determinations and permits for our records.

Sincerely yours,

Bruce P. Miller

Bruce P. Miller, Chief
Air Programs Branch
Air, Pesticides, and Toxics
Management Division

Copied: CHF/BT

Barry Andrews
Jan Rogers

} 11/6/87

HILLSBOROUGH COUNTY
RESOURCE RECOVERY FACILITY
METHOD 8 RETEST
JUNE 16, 1987

Prepared For:

OGDEN PROJECTS, INC.
WATERGATE TOWER I, SUITE 400
1900 POWELL STREET
EMERYVILLE, CA 94608

Prepared By:

ENVIRONMENTAL ENGINEERING CONSULTANTS, INC.
5119 NORTH FLORIDA AVENUE
TAMPA, FLORIDA 33603

June 24, 1987

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I. SUMMARY

On June 16, 1987, Environmental Engineering Consultants, Inc. conducted a retest of emissions at the Hillsborough County Resource Recovery Facility in Tampa, Florida. The source tested was the No. 1 steam boiler burning municipal garbage to generate electricity.

Compliance with specified emissions limits was determined using Method 8 for sulfuric acid mist. Carbon monoxide levels were determined using EPA Method 10 to demonstrate normal combustion conditions.

The testing was performed as specified in the Ogden Projects, Inc. source test plan. Carbon monoxide and sulfuric acid mist/sulfur dioxide tests were conducted on a single boiler taken as representative of the of fuel-related emission levels.

The tests were conducted by Carl Fink, Jack Fross, Byron Burrows, and James Root of Environmental Engineering Consultants, Inc. with the assistance and cooperation of Ogden Projects, Inc. and the employees of the Hillsborough County Resource Recovery Facility.

During testing the boiler was operating at $\pm 10\%$ of its rated capacity.

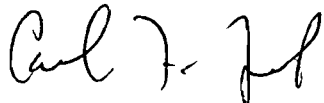
A summary of the test results is shown in Tables 1 and 2. The average sulfuric acid mist concentration was 0.0052 grains per dry standard cubic foot, corrected to 12% CO₂ (gr/dscf-12%). The current permitted concentration is 0.0040 gr/dscf-12%. The average carbon monoxide concentration was 0.002 gr/dscf-12%. The permitted concentration is 0.093 gr/dscf-12%.

The permitted concentration for sulfuric acid mist was exceeded in this emissions test. The carbon monoxide concentrations indicated normal combustion levels.

I hereby certify that these results are true and correct and were obtained by the procedures and methods described herein.

Respectfully Submitted;

ENVIRONMENTAL ENGINEERING CONSULTANTS, INC.



Carl F. Fink
Test Team Leader
Senior Air Pollution Engineer

TABLE 1
TEST SUMMATION

PLANT: Hillsborough County Resource Recovery
 SOURCE: Boiler No. 1
 DATE: June 16, 1987
 PARAMETER: Sulfuric Acid Mist

Run No.	Sample Vol. (DSCF)	Flow Rate (ACFM)	Flow Rate (DSCFM)	H2O (%)	Isokinetics (%)	Stack Temp. (°F)	Carbon Dioxide (%)	Acid Mist Concentration (gr/dscf-12%)	Acid Mist Emissions (lb/hr)
1	48.573	89,227	46,156	16.38	98.7	390	9.6	0.0071	2.25
2	46.620	84,425	43,041	16.77	101.6	397	9.9	0.0052	1.59
3	47.568	85,757	43,671	16.24	105.0	404	9.6	0.0033	0.97
Average		86,470	44,289	16.46	101.8	397	9.7	0.0052	1.60

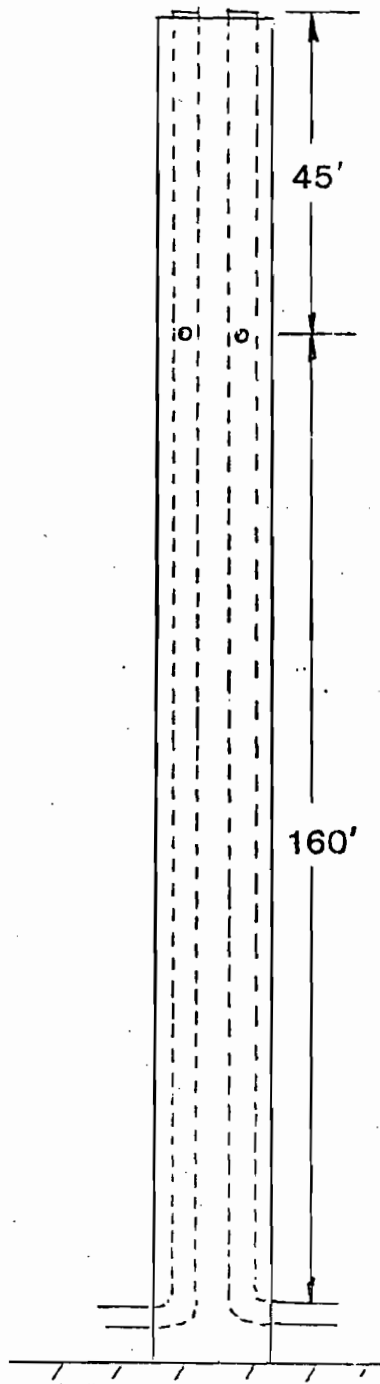
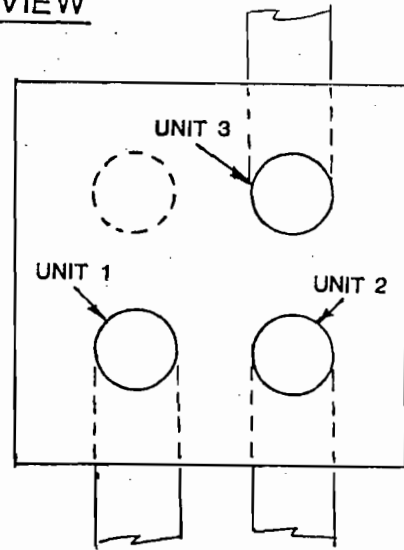
TABLE 2
TEST SUMMATION

PLANT: Hillsborough County Resource Recovery

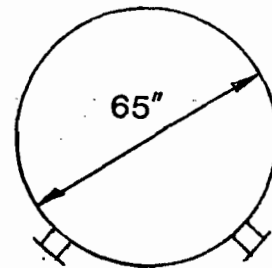
PARAMETER: Carbon Monoxide (CO)

Source/Date	Run Number	Carbon Dioxide (%)	CO Concentration (ppm)	CO Concentration (gr/DSCF-12%)	CO (lb/hr)
Boiler No. 1 June 16, 1987	1	9.6	4.1	.0026	0.81
	2	9.9	2.6	.0016	0.48
	3	9.6	2.7	.0017	0.51
Average				.0020	0.60

TOP VIEW



STACK CROSS SECTION



<u>SAMPLING POINT NUMBER</u>	<u>DISTANCE FROM STACK WALL (IN.)</u>
1	2.86
2	9.49
3	19.24
4	45.76
5	55.51
6	62.14

HILLSBOROUGH CO. RESOURCE RECOVERY
SAMPLING POINT LOCATIONS

ENVIRONMENTAL ENGINEERING
CONSULTANTS, INC.
CONSULTING ENGINEERS &
ENVIRONMENTAL SCIENTISTS

Figure 1

II. SOURCE DESCRIPTION

The Hillsborough County Resource Recovery Facility is located on Faulkenburg Road in Tampa, Florida. Municipal garbage from Hillsborough County is delivered to the facility and charged into three combustion units each firing a boiler to produce steam at a rate of approximately 95,000 pounds per hour. The steam produced drives a turbine generator to produce electricity which is sold to Tampa Electric Company for use in its distribution system.

The exhaust gases from each boiler pass through a separate electrostatic precipitator for particulate matter removal before being vented through separate 65 inch diameter ducts and exhausted at an elevation of 220 ft. The two sampling ports in each duct are located at a point 8.3 stack diameters upstream and 29.5 stack diameter downstream from disturbances in the exhaust flow (see Figure 1). For the continuous measurement type sampling (Method 8) sample ports located as close to ground level as possible were utilized in each of the three ducts.

III. METHODS AND PROCEDURES

CARBON MONOXIDE: EPA Method 10

The Method 10 sampling system was assembled as shown in Figure 2 for each carbon monoxide test. A gas sample was continuously extracted from the duct through a heated pyrex glass probe, heated filter, and teflon tubing to a condenser to remove moisture. After moisture removal the gas was conveyed through teflon tubing to a sample manifold for distributing sample gas at suitable pressure to the appropriate analyzer and for introducing calibration gases directly to the analyzer.

The CO analyzer used was a Thermo Electron Model 48 nondispersive infrared (NDIR) type analyzer operated on the 0-50 ppm scale. The CO values were determined from a continuous stripchart recording of the analyzer output.

The analyzer was calibrated on site before testing using NBS reference gas and a gas dilution system, the use of which was approved on site by HCEPC personnel. At the end of each one hour test run and at the completion of the test, a zero and span drift check was performed. All calibrations and zero and calibration checks were within specified limits.

SULFURIC ACID MIST/SULFUR DIOXIDE: EPA Method 8

The Method 8 sampling train was assembled as shown in Figure 3 for each acid mist/sulfur dioxide test. A six foot probe with a heated pyrex glass liner was used for all test runs. Stack temperature measurements were conducted at each point during sampling. An integrated gas sample was collected through a 1/4"

diameter stainless steel probe fixed to the sampling probe assembly.

The first impinger was a standard Greenburg-Smith (G-S) type charged with 100 ml of 80% isopropanol; the second impinger was modified G-S design charged with 100 ml of 3% hydrogen peroxide; the third was a standard G-S type also charged with 100 ml of 3% hydrogen peroxide; and the fourth impinger was modified G-S type charged with approximately 200 grams of indicator grade silica gel. All impingers were weighed to the nearest 0.5 gram after charging for use in determining moisture collected. Crushed ice was placed around the impingers during sampling to maintain the temperature of the gas leaving the last impinger below 68^o F.

A borosilicate glass fiber filter in a glass filter holder was placed between the first and second impingers for final acid mist collection. The filter was not heated.

Leak tests were performed before and after each sampling run by blocking the nozzle inlet. No leakages were observed at vacuum levels equal to or exceeding those experienced during sampling.

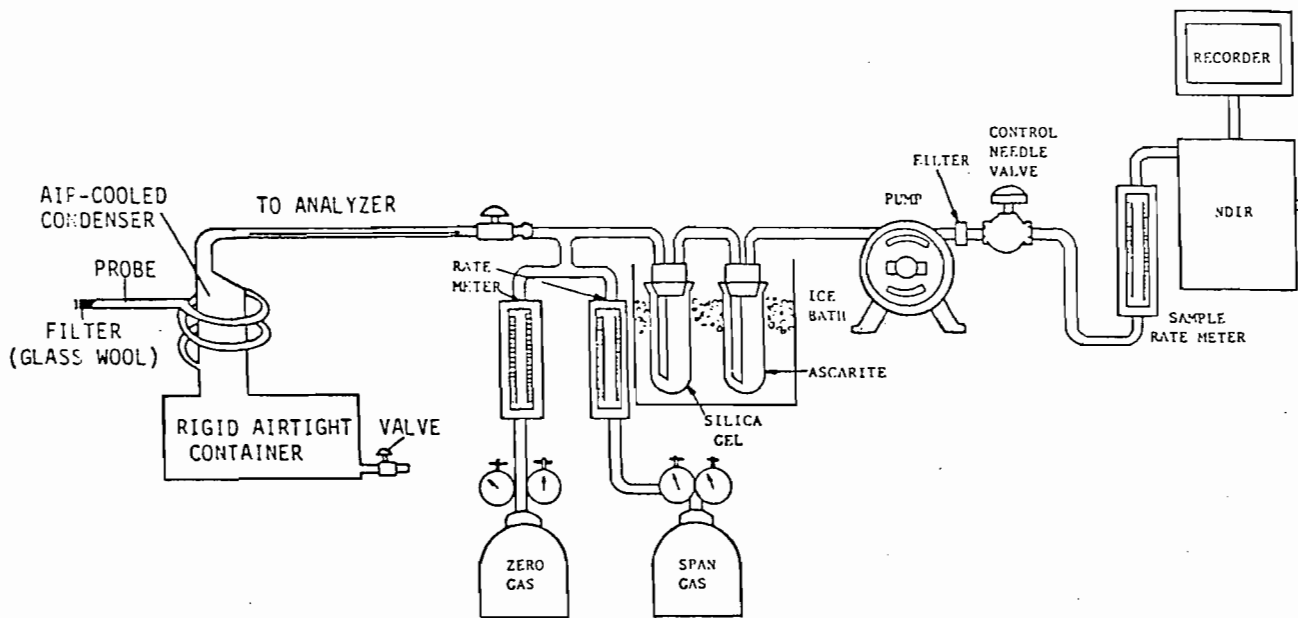
Each sampling run consisted of 12 points, 6 points through each of two ports. Each point was sampled for 5 minutes, giving a total test time of 60 minutes per run.

At the end of each run, after the final leak check, the probe was disconnected, the ice bath drained, and the impingers purged with ambient air for 15 minutes at the average flowrate used in that sampling run. After purging, the impingers were weighed to the nearest 0.5 gram to determine the weight of moisture collected.

The contents of the first impinger and an 80% isopropanol rinse of the nozzle, probe, all glassware before the filter, and the front half of the filter bell were collected in a storage container as the acid mist sample. The filter was removed and added to this container.

The contents of the second and third impingers were transferred to a separate storage container as the sulfur dioxide sample. A distilled water rinse of the second and third impingers and all connecting glassware including the back half of the filter bell was added to this container.

The acid mist analysis was performed at Thornton Laboratories, Inc. under the direction of Mr. Fred Hartledge. The samples were passed through an ion exchange column prior to analysis to eliminate metal ion interference. The analysis was performed utilizing the standard barium-throin titration as described in EPA Method 8.

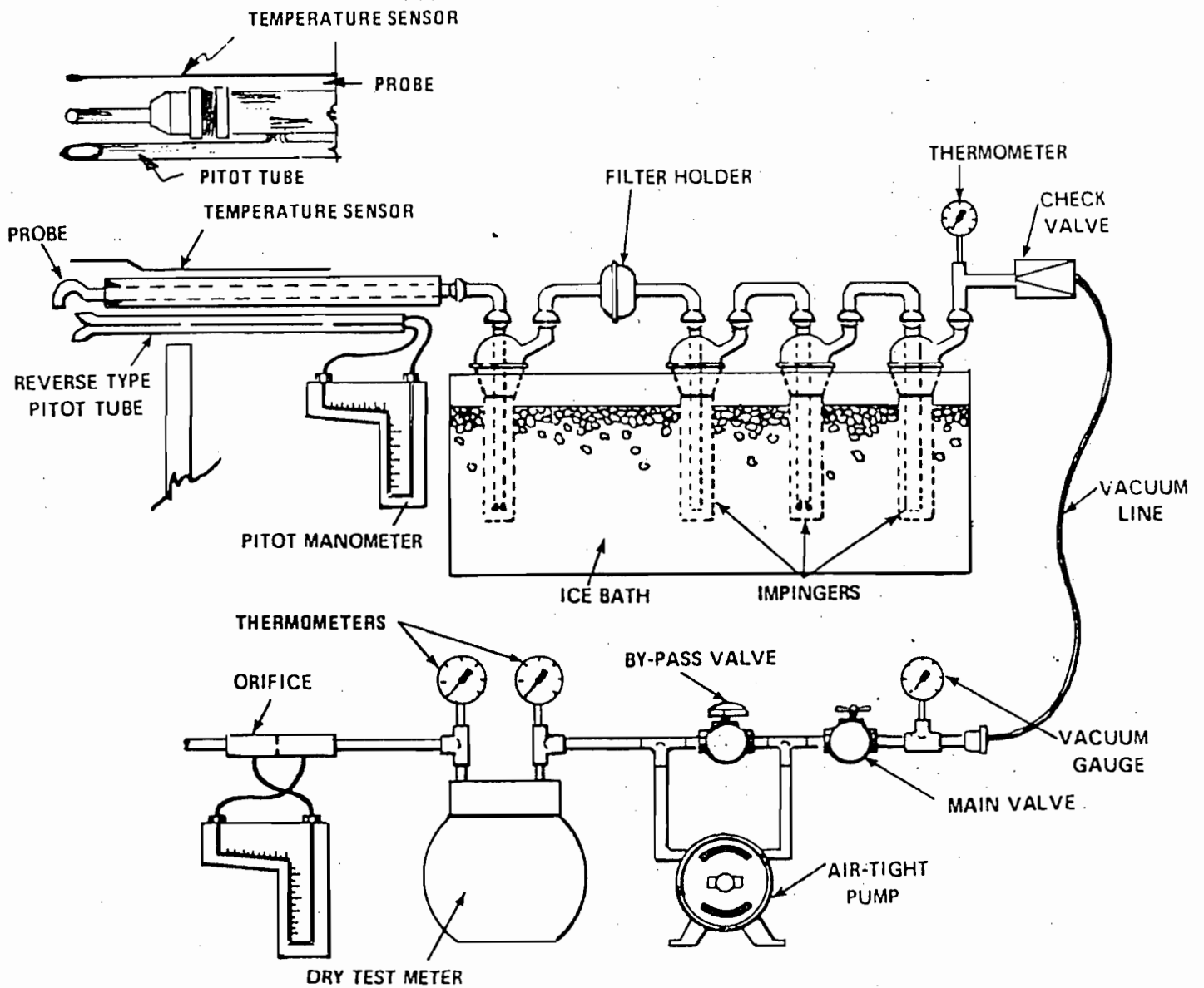


METHOD 10 SAMPLING TRAIN

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CONSULTANTS, INC.

CONSULTING ENGINEERS &
ENVIRONMENTAL SCIENTISTS

Figure 2



METHOD 8 SAMPLING TRAIN

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**CONSULTING ENGINEERS &
ENVIRONMENTAL SCIENTISTS**

Figure 3

APPENDIX A

DATA SUMMARIES AND CALCULATIONS

SOURCE TESTING NOMENCLATURE AND DIMENSIONS

An:	Cross sectional area of nozzle, ft ²
As:	Cross sectional area of stack, ft ²
Bws:	Water vapor in the gas stream, proportion by volume
Cs:	Concentration of particulate matter in stack gas at standard conditions, gr/dscf
Cp:	Pitot tube coefficient
E:	Source emission rate, lbs/hr
I:	Percent of isokinetic sampling
Md:	Molecular weight of stack gas, dry basis, lb/lb-mole
Ms:	Molecular weight of stack gas, wet basis, lb/lb-mole
Mn:	Total particulate collected, less acetone blank correction; grams
Pb:	Barometric pressure at test site, in. Hg
Ps:	Absolute stack gas pressure, in. Hg
Qs:	Volumetric flow rate, dry at standard conditons, SCFM
Tm:	Absolute average dry gas meter temperature, °R
Ts:	Absolute average stack gas temperature, °R
Vlc:	Total volume of liquid collected in impingers and silica gel, ml
Vm:	Volume of gas sampled under actual conditons, DCF
Vm(std):	Volume of gas sampled corrected to standard conditions, DSCF

Vs: Stack gas velocity, ft/sec

Vw: Volume of water in sample corrected to standard conditions, DSCF

Y: Dry gas meter calibration factor

θ: Total sampling time, min.

\hat{P} : Velocity head, in H₂O

\hat{H} : Average pressure differential across orifice meter, in. H₂O

SUMMARY OF TEST DATA

Plant: Hillsborough County
Resource Recovery

Source: Boiler No. 1

Date: June 16, 1987

Parameter: Sulfur Dioxide
/Acid Mist

	Run 1	Run 2	Run 3
Time Interval:	1000-1102	1158-1300	1353-1455
Test Time, min.:	60	60	60
Stack Area, Sq. ft.:	23.044	23.044	23.044
Nozzle Diameter, in.:	0.274	0.274	0.274
Barometric Pressure, in. Hg.:	29.86	29.84	29.84
Absolute Stack Pressure, in. Hg.:	29.82	29.77	29.79
Volume Liquid Collected, ml:	202.0	199.5	195.8
Stack Gas Moisture Content, %:	16.38	16.77	16.24
Stack Gas Temperature, F:	390	397	404
Sample Volume, DSCF:	48.573	46.620	47.568
Gas Velocity, FPS:	64.534	61.061	62.024
Gas Flowrate, ACFM:	89,227	84,425	85,757
Gas Flowrate, DSCFM:	46,156	43,041	43,671
Percent Isokinetic %:	98.7	101.6	105.0
Percent CO ₂ , Volume:	9.6	9.9	9.6
Percent O ₂ , Volume:	9.7	9.4	10.0
Acid Mist collected, g.:	0.018	0.013	0.008
Acid Mist conc., gr/DSCF-12%:	0.0071	0.0052	0.0033
Acid Mist emissions, lb/hr.:	2.25	1.59	0.97

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PLANT HILLSBOROUGH COUNTY RESOURCE RECOVERY

SOURCE BOILER #1

DATE 6-16-87

RUN NO. 1

CALIBRATION

C_p .84

Y 1.050

D_n 0.274 in.

A_n $4.095 \times 10^{-4} \text{ ft}^2$

NEW DATA

P_b 29.86 in. Hg.

P_s 29.82 in. Hg.

A_s 23.044 ft²

θ 60 min.

V_m 49.721 DCF

ΔH 2.77 in. H₂O

T_m 570 °R

T_s 850 °R

V_{ic} 202.0 ml

$(\sqrt{\Delta P})_{avg}$.8902

M_n 0.017 g.

$$V_{m(std)} = \frac{17.64 V_m Y (P_b + \Delta H/13.6)}{T_m} =$$

$$\frac{17.64 (49.721) (1.050) (29.86 + \frac{2.77}{13.6})}{(570)} = 48.573 \text{ DSCF}$$

$$V_w = 0.0471 V_{ic} = 0.0471 (202.0) = 9.5142 \text{ SCF}$$

$$B_{ws} = \frac{V_w}{V_w + V_{m(std)}} = \frac{(9.5142)}{(9.5142) + (48.573)} = 0.1638$$

$$M_d = 0.44(\% \text{ CO}_2) + 0.32(\% \text{ O}_2) + 0.28(200 + 80 \text{ N}_2) =$$

$$0.44(9.6) + 0.32(9.7) + 0.28(80.7) = 29.924$$

$$M_s = M_d(1 - B_{ws}) + 18 B_{ws} = (29.924)(.8362) + 18(.1638) = 27.9708$$

$$V_s = 85.49 C_p (\sqrt{\Delta P})_{avg} (T_s / P_s M_s)^{1/2} =$$

$$85.49 (.84) (.8902) \left[\frac{(850)}{(29.82)(27.9708)} \right]^{1/2} = 64.5335 \text{ FPS}$$

$$Q_s = 1058 (1 - B_{ws}) V_s A_s (P_s / T_s) =$$

$$1058 (.8362) (64.5335) (23.044) \frac{(29.82)}{(850)} = \frac{46.156 \text{ DSCFM}}{69,227 \text{ ACFM}}$$

$$I = \frac{100 V_{m(std)} A_s}{\theta Q_s A_n} = \frac{100 (48.573) (23.044)}{(60) (46.156) (4.095 \times 10^{-4})} = 98.7 \%$$

$$C_s = 15.43 \frac{M_n}{V_{m(std)}} = \frac{(15.43) (.017)}{(48.573)} = 0.0057 \text{ g/DSCF}$$

$$E = \frac{C_s Q_s}{116.67} = \frac{(0.0057) (46.156)}{116.67} = 2.25 \text{ LB/HR}$$

$$C_{s12} = C_s \left(\frac{12}{30.2} \right)$$

$$= 0.0071$$

SOURCE SAMPLING
CALCULATION SHEET

ENVIRONMENTAL ENGINEERING
CONSULTANTS, INC.

CONSULTING ENGINEERS,
ENVIRONMENTAL SCIENTISTS

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PLANT

SOURCE BOILER #1

DATE 6-16-87

RUN NO. 2

CALIBRATION

C_p .84

Y 1.050

D_n 0.274 in.

A_n 4.095 x 10⁻⁷ ft²

NEW DATA

P_b 29.84 in. Hg.

P_s 29.77 in. Hg.

A_s 23.044 ft²

θ 60 min.

V_m 47.768 DCF

ΔH 2.45 in. H₂O

T_m 574 °R

T_s 257 °R

V_{ic} 199.5 ml

(ΔP)_{avg} .8379

M_n g.

$$V_{m(Std)} = \frac{17.64 V_m Y (P_b + \Delta H / 13.6)}{T_m} =$$

$$\frac{17.64 (47.768) (1.050) (29.84 + \frac{2.45}{13.6})}{(574)} = \underline{46.620 \text{ DSCF}}$$

$$V_w = 0.0471 V_{ic} = 0.0471 (199.5) = \underline{9.3965 \text{ SCF}}$$

$$B_{ws} = \frac{V_w}{V_w + V_{m(Std)}} = \frac{(9.3965)}{(9.3965) + (46.620)} = \underline{.1677}$$

$$M_d = 0.44(\% \text{CO}_2) + 0.32(\% \text{O}_2) + 0.28(2\text{CO} + \% \text{N}_2) =$$

$$0.44(9.9) + 0.32(9.4) + 0.28(80.7) = \underline{29.96}$$

$$M_s = M_d(1 - B_{ws}) + 18 B_{ws} = (29.96)(.8323) + 18(.1677) = \underline{27.9543}$$

$$V_s = 85.49 C_p (\sqrt{\Delta P})_{avg} (T_s / P_s M_s)^{1/2} =$$

$$85.49 (.84) (.8379) \left[\frac{(857)}{(29.77)(27.9543)} \right]^{1/2} = \underline{61.061 \text{ FPS}}$$

$$Q_s = 1058 (1 - B_{ws}) V_s A_s (P_s / T_s) =$$

$$1058 (.8323) (61.061) (23.044) \frac{(29.77)}{(857)} = \frac{43,041 \text{ DSCFM}}{84,425 \text{ ACFM}}$$

$$I = \frac{100 V_{m(Std)} A_s}{\theta Q_s A_n} = \frac{100 (46.620) (23.044)}{(60) (43,041) (4.095 \times 10^{-7})} = \underline{101.6 \%}$$

$$C_s = 15.43 \frac{M_n}{V_{m(Std)}} = \frac{(15.43) (.013)}{(46.620)} = \underline{0.0043 \text{ g/DSCF}}$$

$$E = \frac{C_s Q_s}{116.67} = \frac{(0.0043) (43,041)}{116.67} = \underline{1.57 \text{ LB/HR}}$$

C_{s2} = C_s ($\frac{R}{200}$)
 = 0.0052

SOURCE SAMPLING
 CALCULATION SHEET

ENVIRONMENTAL ENGINEERING
 CONSULTANTS, INC.
 CONSULTING ENGINEERS,
 ENVIRONMENTAL SCIENTISTS

Best Available Copy

PLANT HILLSBOROUGH
COUNTY
WASTEWATER
RECOVERY

SOURCE Boiler #1

DATE C-16-87

RUN NO. 3

CALIBRATION

C_p .84

Y 1.050

D_n .274 in.

A_n $4.095 \times 10^{-4} \text{ ft}^2$

NEW DATA

P_b 29.84 in. Hg.

P_s 29.79 in. Hg.

A_s 23.044 ft²

θ 60 min.

V_m 48.913 DCF

ΔH 2.54 in. H₂O

T_m 576 OR

T_s 864 OR

V_{ic} 195.8 ml

$(\sqrt{\Delta P})_{avg}$.8486

M_n 0.008 g.

$$V_{m(std)} = \frac{17.64 V_m Y (P_b + \Delta H/13.6)}{T_m} =$$

$$\frac{17.64 (48.913) (1.050) (29.84 + \frac{2.54}{13.6})}{(576)} = 47.568 \text{ DSCF}$$

$$V_w = 0.0471 V_{ic} = 0.0471 (195.8) = 9.2222 \text{ SCF}$$

$$B_{ws} = \frac{V_w}{V_w + V_{m(std)}} = \frac{(9.2222)}{(9.2222) + (47.568)} = .1624$$

$$M_d = 0.44 (\% \text{ CO}_2) + 0.32 (\% \text{ O}_2) + 0.28 (2\% \text{ CO} + 8\% \text{ N}_2) =$$

$$0.44 (9.6) + 0.32 (10.0) + 0.28 (80.4) = 29.936$$

$$M_s = M_d (1 - B_{ws}) + 18 B_{ws} = (29.936) (.8376) + 18 (.1624) = 27.9976$$

$$V_s = 85.49 C_p (\sqrt{\Delta P})_{avg} (T_s / P_s M_s)^{1/2} =$$

$$85.49 (.84) (.8486) \left[\frac{(864)}{(29.79)(27.9976)} \right]^{1/2} = 62.024 \text{ FPS}$$

$$Q_s = 1058 (1 - B_{ws}) V_s A_s (P_s / T_s) =$$

$$1058 (.8376) (62.024) (23.044) \frac{(29.79)}{(864)} = \frac{43671 \text{ DSCFM}}{85757 \text{ ACFM}}$$

$$I = \frac{100 V_{m(std)} A_s}{\theta Q_s A_n} = \frac{100 (48.913) (23.044)}{(60) (43671) (4.095 \times 10^{-4})} = 105.0 \%$$

$$C_s = 15.43 \frac{M_n}{V_{m(std)}} = \frac{(15.43) (.008)}{(47.568)} = 2.0026 \text{ g/DSCF}$$

$$E = \frac{C_s Q_s}{116.67} = \frac{(2.0026) (43671)}{116.67} = 7477 \text{ LB/HR}$$

$$C_{12} = C_s \left(\frac{12}{6.25} \right)$$

$$= 0.0233$$

SOURCE SAMPLING
CALCULATION SHEET

ENVIRONMENTAL ENGINEERING
CONSULTANTS, INC.

CONSULTING ENGINEERS,
ENVIRONMENTAL SCIENTISTS

APPENDIX B

FIELD AND LABORATORY DATA SHEETS

FIELD DATA LOG

Best Available Copy

PLANT HILLSBOROUGH COUNTY RESOURCE RECOVERY 1

SOURCE Boiler #1

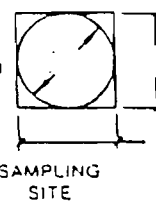
SCHEMATIC OF STACK

NOZZLE I.D. NO. <u>9</u>
DIA 1 <u>.276</u>
DIA 2 <u>.273</u>
DIA 3 <u>.274</u>
AVERAGE <u>.274</u>

RUN NO 1
 DATE 6-16-87
 OPERATORS BURROWS & ROSE
 METER BOX NO EEC-2
 FILTER NO N/A

BAROMETRIC PRESSURE 29.86
 STATIC PRESSURE ---
 AMBIENT TEMPERATURE 105°F
 PROBE LENGTH 6 FT.
 PROBE LINER Pyrex
 PORT LENGTH 8 1/2"

CROSS SECTION



SAMPLING SITE

PORT LOCATION

NOMOGRAPH VALUES	
$\Delta H @$ _____	C FACTOR _____
T_m _____	AVG ΔP _____
W_{H_2O} _____	T_1 _____
REFERENCE <u>3.15</u>	

FINAL VOLUME <u>252.521</u>
INITIAL VOLUME <u>202.800</u>
NET VOLUME <u>49.721</u>

METER SYSTEM LEAK-CHECK OK @ 15" Hg
 ORSAT LEAK-CHECK
 SAMPLE BAG LEAK-CHECK

TRAVERSE POINT NUMBER	SAMPLING TIME		STACK TEMP (t) °F	VELOCITY HEAD		ORIFICE METER (ΔH)	GAS SAMPLE VOLUME (V _m) ft ³	DRY GAS METER TEMP (T _m) °F	PROBE TEMP °F	SAMPLE BOX TEMP °F	TEMP OF GAS LEAVING LAST IMPINGER °F	PUMP VACUUM GAUGE in. Hg
	CLOCK	SAMPLE		(ΔP _s)	(√ΔP _s)							
	1000	0										
1		5	406	.93		3.26	207.10	106		221	56	9
2		10	406	.88		3.08	211.75	106		230	60	9
3		15	408	1.00		3.50	215.99	108		219	60	10
4		20	407	.85		2.93	220.30	109		219	60	8
5		25	407	.75		2.59	224.90	109		218	60	6
6		30	281	.43		1.48	227.53	110		217	65	4
1		35	404	.76		2.62	231.55	110		215	67	7
2		40	405	.87		3.00	235.73	111		221	62	8
3		45	405	.85		2.93	240.00	111		221	62	8
4		50	406	.89		3.07	244.65	112		222	62	8
5		55	406	.89		2.86	248.78	113		221	61	8
6		60	335	.57		1.97	252.521	113		221	59	5
	1102											
			4676	10.6821		33.29		1318				
			390					116				
			850'R	0.8902		2.77		570				
TOTAL												
AVERAGE												

STATIC PITOT LEAK-CHECK @ 15 sec <input checked="" type="checkbox"/>
IMPACT PITOT LEAK-CHECK @ 15 sec <input checked="" type="checkbox"/>
TRAIN LEAK RATE @ 60 sec 0.00 cf @ 10 in

VOLUME OF LIQUID WATER COLLECTED	IMPINGER WEIGHT (g) OR VOLUME (mm)			
	1	2	3	4
FINAL	67.4	56.1	56.1	56.1
INITIAL	55.3	55.7	57.3	57.7
LIQUID COLL.	12.1	6.4	0.8	0.4
TOTAL VOLUME				

TIME	GAS MEASUREMENTS			
	CO ₂	O ₂	CO	N ₂
1	9.6	9.5		
2	9.3	9.7		
3	9.7	9.7		
4	AVG 9.3	9.7		180.7

ENVIRONMENTAL ENGINEERING CONSULTANTS, INC.

SIGNATURE

TEST TEAM CHIEF

Carl U

FIELD DATA LOG

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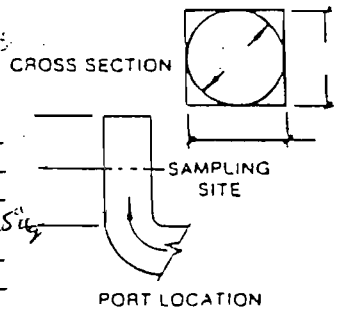
PLANT HILLSBOROUGH COUNTY RESOURCE RECOVERY SOURCE ROLLER #1

SCHEMATIC OF STACK

NOZZLE I.D. NO. 9
 DIA 1 _____
 DIA 2 _____
 DIA 3 _____
 AVERAGE 274

RUN NO. 2
 DATE 6-16-87
 OPERATORS BURGESS & WOT
 METER BOX NO. EEC-2
 FILTER NO. N/A

BAROMETRIC PRESSURE 29.84
 STATIC PRESSURE -0.92 in. H₂O
 AMBIENT TEMPERATURE 105°F
 PROBE LENGTH 6 FT
 PROBE LINER PYREX
 PORT LENGTH _____
 PORT DIAMETER _____
 METER SYSTEM LEAK-CHECK OK
 ORSAT LEAK-CHECK OK
 SAMPLE BAG LEAK-CHECK ✓



NOMOGRAPH VALUES
 ΔH@ _____ C FACTOR _____
 T_m _____ AVG ΔP _____
 W_{H2O} _____ T_s _____
 REFERENCE K=3.53

FINAL VOLUME 312.768
 INITIAL VOLUME 265.000
 NET VOLUME 47.768

TRAVERSE POINT NUMBER	SAMPLING TIME		STACK TEMP (T _s) °F	VELOCITY HEAD		ORIFICE METER (ΔH)	GAS SAMPLE VOLUME (V _m) ft ³	DRY GAS METER TEMP (T _m) °F	PROBE TEMP °F	SAMPLE BOX TEMP °F	TEMP OF GAS LEAVING LAST IMPINGER °F	PUMP VACUUM GAUGE in. Hg
	CLOCK	SAMPLE		(ΔP _s)	(√ΔP _s)							
	1158	0					265.000					
1		5	412	.87		3.00	269.45	111		224	59	7
2		10	412	.87		3.00	273.35	111		222	54	7
3		15	409	.62		2.14	277.66	111		220	61	5
4		20	405	.69		2.38	281.45	112		219	66	6
5		25	405	.69		2.38	285.50	113		221	66	6
6		30	381	.40		1.38	288.59	114		217	66	3
1		35	399	.77		2.66	292.60	114		224	65	6
2		40	400	.83		2.83	296.95	115		226	65	7
3		45	398	.77		2.66	301.00	114		230	65	6
4		50	399	.77		2.66	305.09	116		230	67	6
5		55	399	.70		2.17	309.19	116		230	67	6
6		60	384	.53		1.87	312.768	117		223	67	5
	1300											
			47.63		10.0549	27.43		1364				
			397					114				
			857°R		0.8374	2.4525		574°R				
TOTAL												
AVERAGE												

STATIC PITOT LEAK-CHECK @ 15 sec _____
 IMPACT PITOT LEAK-CHECK @ 15 sec _____
 TRAIL LEAK RATE @ 60 sec 0.00 cf @ 12 in

VOLUME OF LIQUID WATER COLLECTED	IMPINGER WEIGHT (g) OR VOLUME (ml)			
	1	2	3	4
FINAL				
INITIAL				
LIQUID COLL.				
TOTAL VOLUME				

TIME	GAS MEASUREMENTS			
	CO ₂	O ₂	CO	N ₂
1	9.9	7.5		
2	10.0	7.4		
3	7.9	7.4		
4	AVG 9.9	7.4		150.7

ENVIRONMENTAL ENGINEERING CONSULTANTS, INC.

SIGNATURE Carl J.
 TEST TEAM CHIEF

FIELD DATA LOG

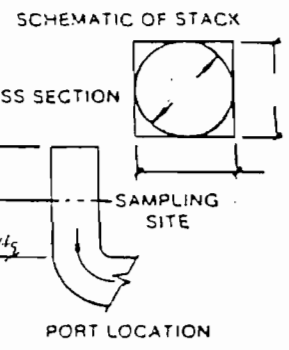
Best Available Copy

PLANT HILLSBOROUGH COUNTY RESOURCE RECOVERY SOURCE BOILER #1

NOZZLE I.D. NO. 9
 DIA 1 _____
 DIA 2 _____
 DIA 3 _____
 AVERAGE 279

RUN NO 3
 DATE 6-16-87
 OPERATORS BURROWS & ROOT
 METER BOX NO EBC-2
 FILTER NO N/A

BAROMETRIC PRESSURE 29.81
 STATIC PRESSURE 2.82
 AMBIENT TEMPERATURE 105°F
 PROBE LENGTH 6 FT.
 PROBE LINER PIREX
 PORT LENGTH _____
 PORT DIAMETER _____
 METER SYSTEM LEAK-CHECK 2.00" @ 15" Hg
 ORSAT LEAK-CHECK
 SAMPLE BAG LEAK-CHECK



NOMOGRAPH VALUES

$\Delta H @$ _____ C FACTOR _____
 T_m _____ AVG ΔP _____
 W_{H_2O} _____ T_s _____
 REFERENCE 353

FINAL VOLUME 374.413
 INITIAL VOLUME 325.500
 NET VOLUME 48.913

TRAVERSE POINT NUMBER	SAMPLING TIME		STACK TEMP (t) °F	VELOCITY HEAD		ORIFICE METER (ΔH)	GAS SAMPLE VOLUME (V _m) ft ³	DRY GAS METER TEMP (t _m) °F	PROBE TEMP °F	SAMPLE BOX TEMP °F	TEMP OF GAS LEAVING LAST IMPINGER °F	PUMP VACUUM GAUGE in. Hg
	CLOCK	SAMPLE		(ΔP) PSI	(√ΔP) PSI							
	1353	0					325.500			202		
1		5	404	.80	2.82	329.60	113			252 202	54	7
2		10	404	.80	2.82	333.79	114			207	54	7
3		15	406	.83	2.93	338.06	114	350		205	63	7
4		20	406	.74	2.61	342.40	114			202	66	7
5		25	405	.69	2.44	346.65	116			200	64	6
6		30	381 402	.64	2.26	350.50	116	221		203	65	6
1		35	406	.80	2.82	354.75	116			224	65	7
2		40	406	.70	2.40	358.65	116			224	66	6
3		45	405	.67	2.37	362.58	117			230	67	6
4		50	403	.70	2.47	366.66	117	254		226	60	6
5		55	402	.67	2.33	370.60	117			227	60	6
6		60	398	.62	2.19	374.413	118	225		226	61	6
	1455											
			4847		10.830	30.46		1388				
			404					116				
			864°R		0.5986	2.5385		576°K				
TOTAL												
AVERAGE												

STATIC PITOT LEAK-CHECK @ 15 sec
 IMPACT PITOT LEAK-CHECK @ 15 sec
 TRAIN LEAK RATE @ 50 sec _____ cf @ _____ in

VOLUME OF LIQUID WATER COLLECTED	IMPINGER WEIGHT (g) OR VOLUME (ml)			
	1	2	3	4
FINAL	630.7	608.0	584.4	310.0
INITIAL	594.7	555.4	522.2	250.0
LIQUID COLL.	36.0	52.6	62.2	60.0
TOTAL VOLUME		195.2		

TIME	GAS MEASUREMENTS			
	CO ₂	O ₂	CO	N ₂
1	9.5	10.0		
2	9.3	10.0		
3	9.0	9.9		
4	AVE 9.5	10.0		30.4

ENVIRONMENTAL ENGINEERING CONSULTANTS, INC.

PHONE - 374 52
 385.05

SIGNATURE Carl J. Root
 TEST TEAM CHIEF

THORNTON LABORATORIES, INC.

TWX 810 876-9134
THORNT LAB TPA

1145 EAST CASS STREET
TAMPA, FLORIDA 33601 - 2880
MARINE, ANALYTICAL AND ENVIRONMENTAL SERVICES

TELEPHONE (813) 223-9702
P.O. BOX 2880

June 24, 1987

Laboratory Number 662469-662472
Sample of Stack Solution
Date Received June 17, 1987
For Environmental Engineering Consultants
P.O. Box 7854
Tampa, Florida 33673
Attention Carl Fink
Marks: See Below

CERTIFICATE OF ANALYSIS

<u>LABORATORY NUMBER</u>	<u>MARKS</u>	<u>SO₂ (EPA Method 8)</u>
662469	Blank, 80% Isopropanol, 6/16/87	0.0008 grams
662470	Boiler #1, Run #1, 6/16/87, Alcohol Wash	0.019 grams
662471	Boiler #1, Run #2, 6/16/87, Alcohol Wash	0.014 grams
662472	Boiler #1, Run #3, 6/16/87, Alcohol Wash	0.009 grams

LABORATORY ID #E4147 and TB4100

THORNTON LABORATORIES, INC.

Best Available Copy

THORNTON LABORATORIES, INC.

TWX 810 876-9134
THORNT LAB TPA

1145 EAST CASS STREET
TAMPA, FLORIDA 33601 - 2880
MARINE, ANALYTICAL AND ENVIRONMENTAL SERVICES

TELEPHONE (813) 223-9702
P.O. BOX 2880

June 24, 1987

Laboratory Number 662473-662474
Sample of Stack Solution
Date Received June 17, 1987
For Environmental Engineering Consultants
P.O. Box 7854
Tampa, Florida 33673
Attention Carl Fink
Marks: See Below

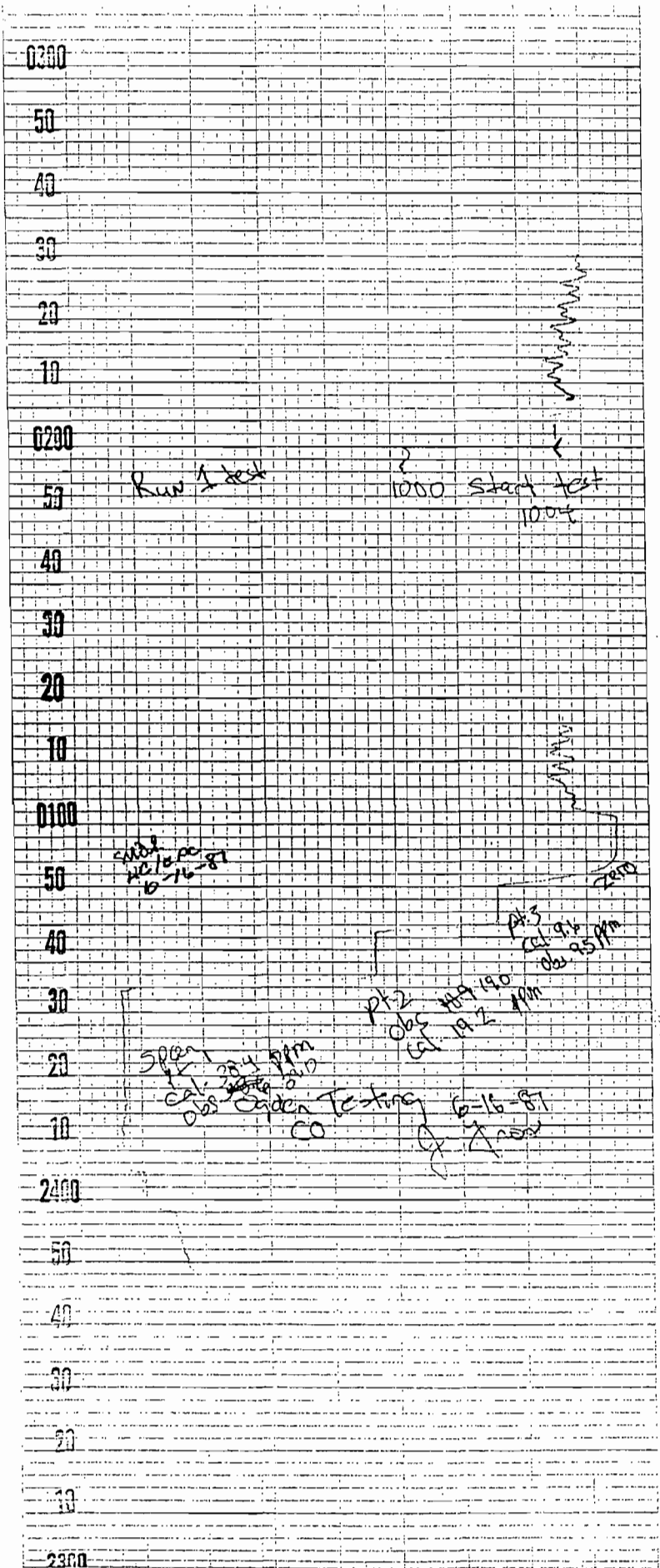
CERTIFICATE OF ANALYSIS

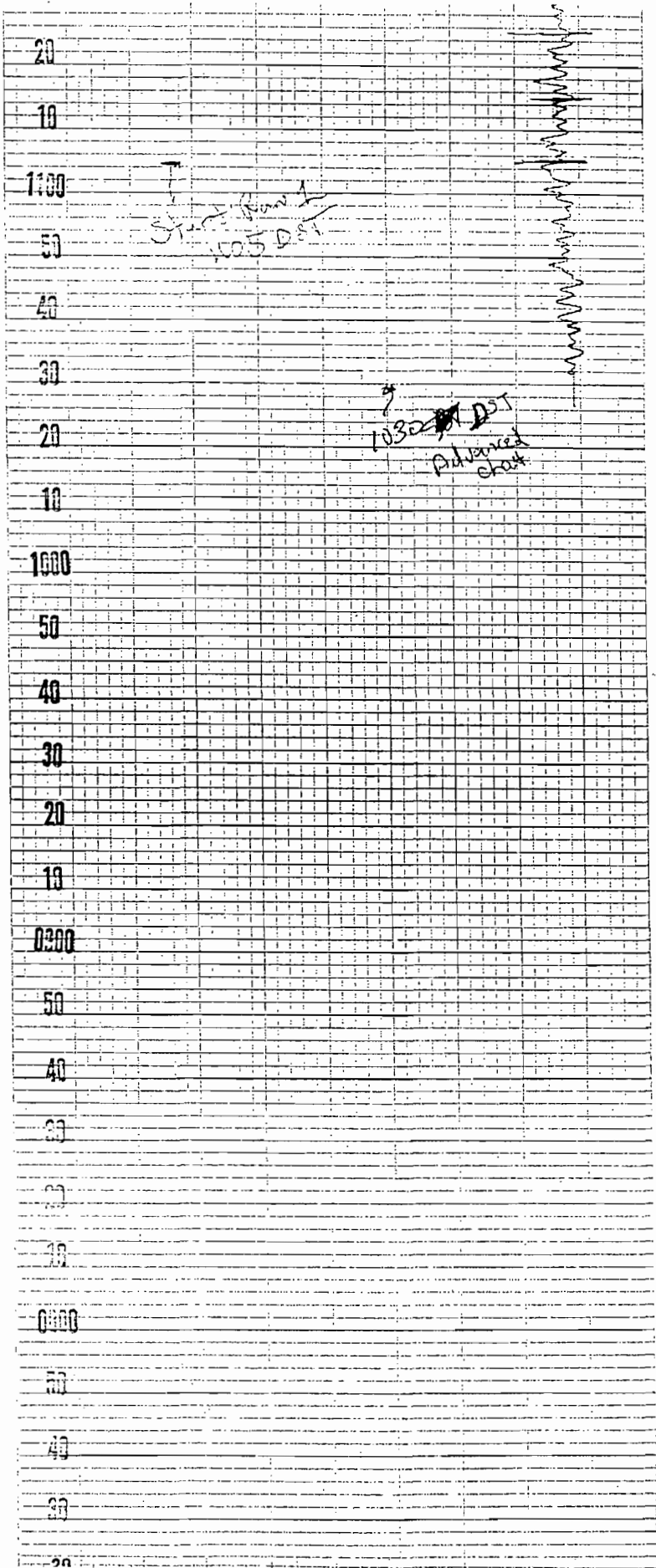
<u>LABORATORY NUMBER</u>	<u>MARKS</u>	<u>SO₂ (EPA Method 8)</u>
662473	EPA Compliance Audit A00401	1.53 g/dscm
662474	EPA Compliance Audit A02804	0.72 g/dscm

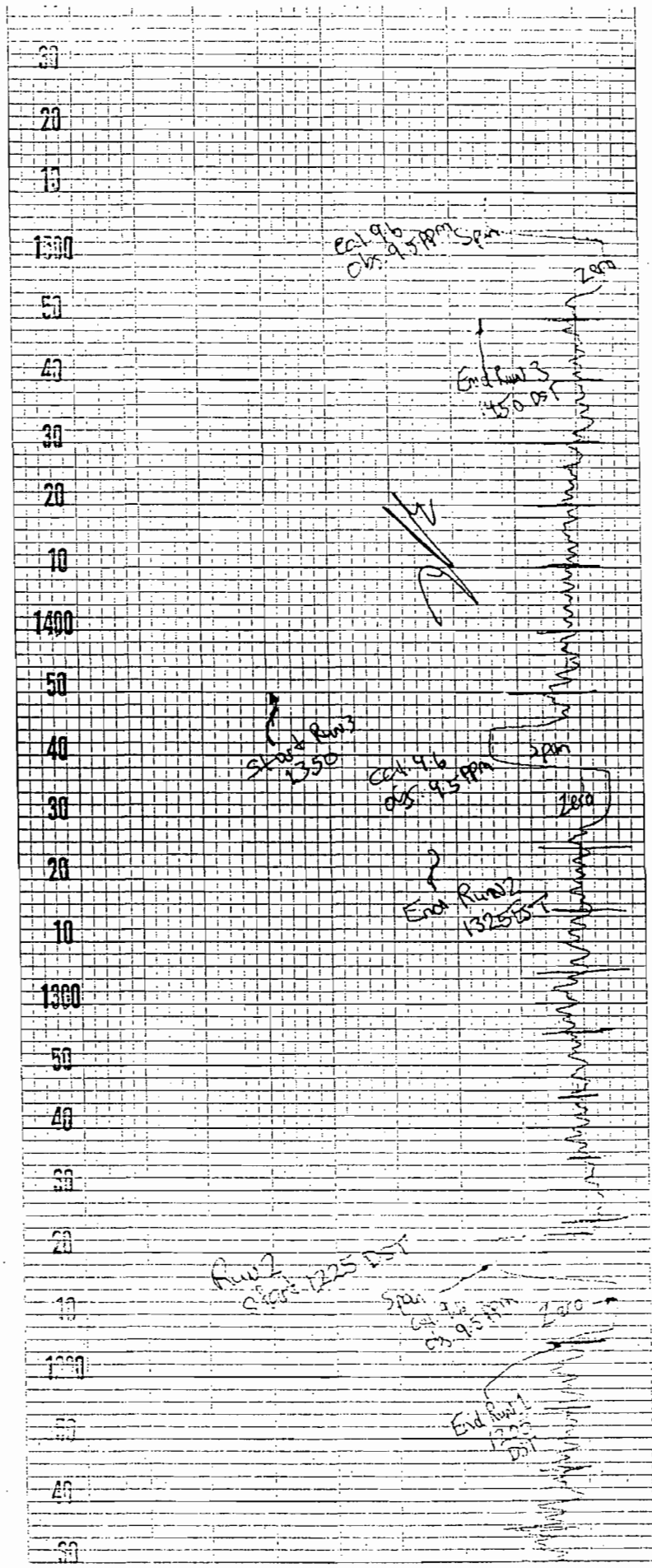
LABORATORY ID #E4147 and T84100

THORNTON LABORATORIES, INC.









APPENDIX C
CALIBRATION DATA

SUMMARY OF EQUIPMENT CALIBRATION

<u>Equipment</u>	<u>Calib. Date</u>	<u>Place</u>	<u>Method</u>	<u>Results</u>
Nozzle #9	06-16-87	On-site	3 measurements w/vernier caliper	Dn=0.274 in.
Pitot Tube P-4	02-23-87	EEC, Inc.	EPA Method	Cp=0.84
Meter Console EEC-2	03-30-87	EEC, Inc.	Wet Test Meter	Y=1.050 ^H@=2.09
Post-Test Check	06-18-87	EEC, Inc.	Wet Test Meter	Y=1.036
Thermocouples	02-02-87	EEC, Inc.	Comparison to ASTM Thermometer	Correct to $\pm 1\%$ ($^{\circ}$ R)

ENVIRONMENTAL ENGINEERING CONSULTANTS, INC.

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? X yes no

Pitot tube openings damaged? yes (explain below) X no

$\alpha_1 =$ 1.0 ° (<10°), $\alpha_2 =$ 0 ° (<10°), $\beta_1 =$ 2.0 ° (<5°),

$\beta_2 =$ 2.0 ° (<5°)

$\gamma =$ 1.5 °, $\theta =$ 0 °, $A =$ 2.4 cm (in.)

$z = A \sin \gamma =$ 0.063 cm (in.); <0.32 cm (<1/8 in.),

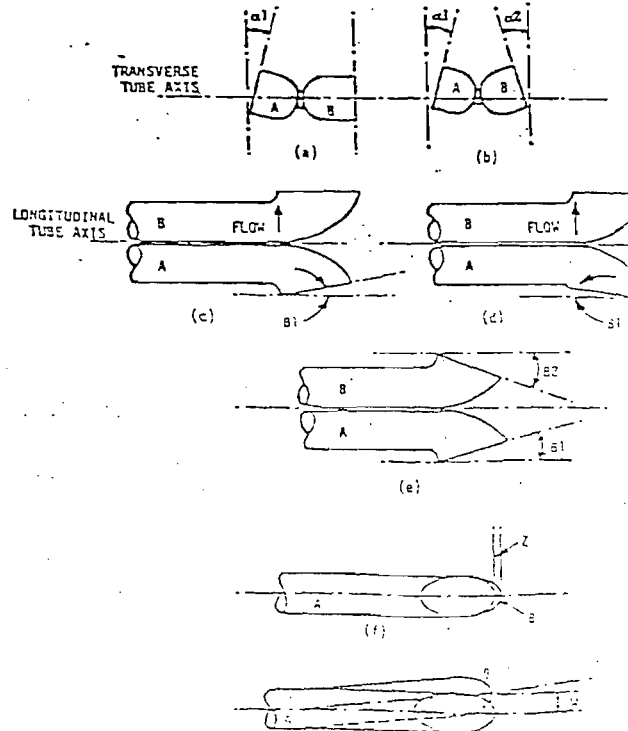
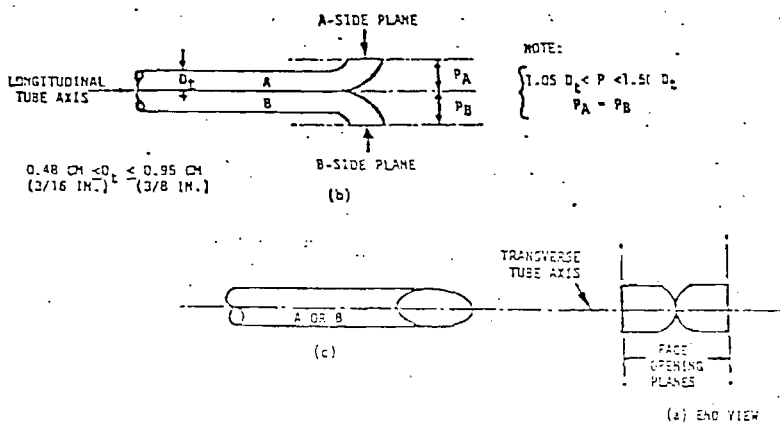
$w = A \sin \theta =$ 0 cm (in.); <.08 cm (<1/32 in.)

$P_A =$ 1.2 cm (in.) $P_B =$ 1.2 cm (in.)

$D_t =$ 0.98 cm (in.)

Comments: _____

Calibration required? yes X no



Pitot tube I.D. Number: P-4

Inspection Date: 2/23/87

Inspected By: [Signature]

Environmental Engineering Consultants, Inc.

METER BOX CALIBRATION DATA AND CALCULATION FORM

Date 3/30/57

Meter box number EEC-2

Barometric pressure, $P_b =$ 29.81 in. Hg

Calibrated by [Signature]

Orifice manometer setting (ΔH), in. H ₂ O	Gas volume		Temperatures				Time (θ), min	Y_i	$\Delta H @_i$, in. H ₂ O
	Wet test meter (V_w), ft ³	Dry gas meter (V_d), ft ³	Wet test meter (t_w), °F	Dry gas meter					
				Inlet (t_{d_i}), °F	Outlet (t_{d_o}), °F	Avg ^a (t_d), °F			
0.5	3.738	3.687	71	78	77	77.5	10	1.025	2.00
1.0	5.206	5.114	71	78	77	77.5	10	1.028	2.06
1.5	6.325	6.145	71	79	77	78	10	1.039	2.09
2.0	7.294	6.931	71	80	78	79	10	1.063	2.09
2.5	8.121	7.648	71	80	78	79	10	1.071	2.11
3.0	8.801	8.252	71	80	78	79	10	1.075	2.16
							Avg	1.050	2.09

ΔH , in. H ₂ O	$\frac{\Delta H}{13.6}$	$Y_i = \frac{V_w P_b (t_d + 460)}{V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\Delta H @_i = \frac{0.0317 \Delta H}{P_b (t_d + 460)} \left[\frac{(t_w + 460) \theta}{V_w} \right]^2$
0.5	0.0368	$Y_1 = \frac{3.738 (29.81) (537.5)}{3.687 (29.847) (531)} = 1.025$	$\Delta H_1 = \frac{0.0317 (0.5)}{29.81 (537.5)} \left[\frac{531 (10)}{3.738} \right]^2 = 1.996$
1.0	0.0737	$Y_2 = \frac{5.206 (29.81) (537.5)}{5.114 (29.834) (531)} = 1.028$	$\Delta H_2 = \frac{0.0317 (1.0)}{29.81 (537.5)} \left[\frac{531 (10)}{5.206} \right]^2 = 2.058$
1.5	0.110	$Y_3 = \frac{6.325 (29.81) (539)}{6.145 (29.92) (531)} = 1.039$	$\Delta H_3 = \frac{0.0317 (1.5)}{29.81 (539)} \left[\frac{531 (10)}{6.325} \right]^2 = 2.090$
2.0	0.147	$Y_4 = \frac{7.294 (29.81) (539)}{6.931 (29.957) (531)} = 1.063$	$\Delta H_4 = \frac{0.0317 (2.0)}{29.81 (539)} \left[\frac{531 (10)}{7.294} \right]^2 = 2.091$
2.5	0.184	$Y_5 = \frac{8.121 (29.81) (539)}{7.648 (29.94) (531)} = 1.071$	$\Delta H_5 = \frac{0.0317 (2.5)}{29.81 (539)} \left[\frac{531 (10)}{8.121} \right]^2 = 2.107$
3.0	0.221	$Y_6 = \frac{8.801 (29.81) (539)}{8.252 (30.031) (531)} = 1.075$	$\Delta H_6 = \frac{0.0317 (3.0)}{29.81 (539)} \left[\frac{531 (10)}{8.801} \right]^2 = 2.155$

^a If there is only one thermometer on the dry gas meter, record the temperature under t_d .

ENVIRONMENTAL ENGINEERING CONSULTANTS, INC.

RECHECK OF ORIFICE AND DGM CALIBRATION

CALIBRATION CHECK BY: B. J. Burman DATE: 6-18-87 CONTROL BOX NO. EEC-2

LEAK CHECK OF METER SYSTEM _____ BAROMETRIC PRESSURE ("Hg) 30.03 09

-ΔHw ("H ₂ O)	ΔHd ("H ₂ O)	Wet Meter Volume (ft ³)	Final Dry Meter Volume (ft ³)	Initial Dry Meter Volume (ft ³)	Net Dry Meter Volume (ft ³)	Wet Test Meter (°F)	Dry Test Meter		Time (Min)	Vacuum Setting ("Hg)
							Inlet (°F)	Outlet (°F)		
X	2.5	8.008	467.771	460.019	7.752	75	91	90	10	10
X	2.5	8.016	475.534	467.771	7.763	75	91	90	10	10
X	2.5	8.010	483.341	475.534	7.807	75	91	90	10	10
01	02	03			04	05	06	07	08	

Perform three calibration runs at a single intermediate orifice meter setting (ΔHd) with the vacuum set at the maximum value reached during the previous test series. If the calibration factor γ deviates by <5% from the initial calibration factor γ, then the dry gas meter volumes obtained during the test series are acceptable. If γ deviates by >5%, recalibrate the metering system, and use whichever meter coefficient (initial or recalibrated) that yields the lowest gas volumes for each test run.

$$\gamma = \frac{V_w (P_b - (\Delta H_w / 13.6)) (t_d + 460)}{V_d (P_b + (\Delta H_d / 13.6)) (t_w + 460)}$$

$$\Delta H_d = 0.0317 (\Delta H) / (P_b (t_d + 460) \times (t_w + 460) \theta / V_w)^2$$

Prior Calibration γ = 1.050

Recheck Calibration γ = 1.036

Δ Difference = -1.4 (If <5%, then use prior calibration γ for calculations.)

STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

Date 2-2-87 Thermocouple number EEC-2 UNIT A
 Ambient temperature 75 °F Barometric pressure _____ in. Hg
 Calibrator ASTM Reference: mercury-in-glass ASTM
Signatures other _____

Reference point number	Source ^a (specify)	Reference thermometer temperature, °F	Thermocouple potentiometer temperature, °F	Temperature difference, °F ^b
1	AMBIENT AIR	75	77	+2
2	ICE BATH	32	36	+4
3	HOT OIL	500	493	-7

^aType of calibration system used.

^b
$$\left[\frac{(\text{ref temp, } ^\circ\text{C} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right] 100 \leq 1.5\%$$

<u>Instrument</u>	<u>Recorder</u>	<u>Calibration System</u>	<u>Mass Flowmeter</u>
Manufacture <u>Thermo Electron</u>	Manufacture <u>ESTERLINE-ANGUS</u>	Manufacture <u>EEC</u>	Manufacture <u>DATAMETRICS</u>
Model No. <u>48</u>	Model No. <u>MS 401 B</u>	Model No. <u>NA</u>	Model No. <u>831</u>
Serial No. <u>48-20608-191</u>	Serial No. <u>S-22087-1A</u>	Serial No. <u>NA</u>	Serial No. <u>1205/545</u>
Range <u>0-50 ppm</u>	Chart Speed <u>6 cm/hr</u>	Type <u>GAS DILUTION</u>	Transducer S/N <u>NA</u>
Zero Pot. <u>738</u>	<u>Digital Multimeter</u>	<u>SO2 Cylinder</u>	Range <u>0-10,000 / 0-50 cc/m</u>
Span Pot. <u>815</u>	Manufacture <u>NLS</u>	Manufacture <u>NBS</u>	<u>Data Logger</u>
Zero (D.L.) <u>NA</u>	Model No. <u>PM450</u>	Cylinder No. <u>FF-20051</u>	Manufacture <u>N/A</u>
% Chart <u>5.0</u>	Serial No. <u>193260/193261</u>	Concentration <u>959</u>	Model # _____
	Calibration Date <u>3-30-87</u>	Expiration Date <u>10-17-88</u>	S/N _____

Level I Span % Diff. _____ Site Name OGDEN TESTING HILLSBOROUGH CO. Date 6-16-87

Point	Dilution Flow (cc/min)	SO Flow (cc/min)	Observed Conc. (ppm)	Calculated Conc. (ppm)	% Diff.
1	1500	0	0.0	0.0	0
2	1200	50	39.0	38.4	+1.6
3	2450	50	19.0	19.2	-1.0
4	4950	50	9.5	9.6	-1.0

Signature *[Handwritten Signature]*

Average _____

Environmental Engineering Consultants, Inc.
Recorder Calibration

Hillsborough County Solid Waste-to-Energy Facility
 Site 210 N. Faulkenburg Rd. Parameter NO_x

Recorder: Manufacturer <u>Esterline Angus</u> Model No. <u>M5401R</u> Serial No. <u>S-22087-1A</u> Range <u>0-1 Volt</u>	VOLTAGE			RECORDER READING	
	Test Point	Unadjusted	Adjusted	% Chart Unadjusted	% Chart Adjusted
Digital Multimeter: Manufacturer <u>Simpson</u> Model No. <u>463</u> Serial No. <u>A15560</u> Calibration Date <u>3-12-87</u>	1	.000		4.9	
Voltage Source: Manufacturer <u>EEC.</u> Model No. <u>NA</u> Serial No. <u>NA</u>	2	.255		30.5	
	3	.555		60.5	
Calibrated By <u>Jack Fox</u> Date <u>4-15-87</u> <u>(on site)</u>	4	.955		100.5	
	5	.753		90.0	
	6	.405		45.0	
	7	.152		20.0	
	8	.000		5.0	
	9				
	10				

National Bureau of Standards
Certificate of Analysis
Standard Reference Material 1681b
Carbon Monoxide in Nitrogen
(Nominal Concentration 1000 ppm)
(Mobile-Source Emission Gas Standard)

This Standard Reference Material is intended for use in the calibration of instruments used for the analysis of carbon monoxide in mobile-source emissions. It is not intended as a working standard, but rather as a primary standard to which the concentration of other standards may be related.

Carbon monoxide concentration: 959 ± 9 μmole/mole (ppm)
Cylinder Number: FF-20051 Sample Number: 1-25-F

The concentration of carbon monoxide is relative to all other constituents of the gas.

The uncertainty shown is the estimated upper limit of error of the carbon monoxide concentration and is the 95 percent confidence interval based on allowances for known sources of possible error.

Each cylinder of gas is individually analyzed, and the concentration given above applies only to the cylinder identified by cylinder number and sample number on this certificate.

The original development and evaluation of the carbon monoxide in nitrogen series of Standard Reference Materials was performed in the Gas and Particulate Science Division by J. M. Ives and W. D. Dorko.

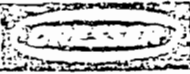
The overall direction and coordination of the technical measurements leading to certification were performed under the chairmanship of E. E. Hughes and H. L. Rook, Chief of the Gas and Particulate Science Division.

The technical and support aspects involved in the preparation, certification, and issuance of this Standard Reference Material were coordinated through the Office of Standard Reference Materials by T. E. Gills.

Washington, D.C. 20234
January 25, 1980

George A. Uriano, Chief
Office of Standard Reference Materials

(over)



DATAMETRICS • DRESSER INDUSTRIES, INC.
 340 FORDHAM ROAD • WILMINGTON, MASS 01887 • (617) 658-5410

CUSTOMER ENVIRONMENTAL ENG JOB NO. R11784 DATE 2-18-87
 MODEL 831-1CL4-AIR-V-4B-X SERIAL NO. 1205 RANGE 10L GAS AIR
 TEST GAS N₂ CORRECTION FOR GAS 0 LINE PSIG 40 PSIG
 TEMP. F 75 BAROMETRIC PRESSURE 29.97⁴⁹ CORRECTION FACTOR _____
 VALVE TYPE _____ SERIAL NO. _____ ORIFICE _____

STANDARD ±.2%

% OF FULL SCALE	831 V _{OUT}	BROOKS VOL-U-METER GAS CALIBRATOR	831 V _{OUT}
0	.000	.000	.000
10	.920	1.000	.994
20		2.000	1.985
30	2.880	3.000	2.989
40		4.000	3.994
50	4.865	5.000	4.998
60	5.874	6.000	6.006
70		7.000	7.013
80	7.861	8.000	8.021
90		9.000	9.017
100	9.821	10.000	10.000
%	V _{DC}	SCCM / <u>SLPM</u>	V _{DC}

AS RECEIVED
 READJUSTED FULL SCALE + R3
 AND UNIT RETURNED TO ORIGINAL CALIBRATION.

AFTER CALIBRATION

COMMENTS:

LINEARIZER TEST POINT (PIN "E") SHOULD NOT BE ADJUSTED.

ONCE R3 HAS BEEN ADJUSTED THIS CURVE IS NO LONGER VALID, AS WELL AS FULL SCALE GAIN CONTROL (R17).

Michael J. Amato
 FLOW TECHNICIAN



DATAMETRICS • DRESSER INDUSTRIES, INC.
340 FORDHAM ROAD • WILMINGTON, MASS. 01897 • (617) 655-5410

CERTIFICATE OF CALIBRATION

CUSTOMER ENVIRONMENTAL ENGINEERING CONSULTANTS
CUSTOMER P.O. 87050
TRANSDUCER MODEL 831-10L4-AIR-V-4B-X
TRANSDUCER SERIAL # 1205

This is to certify that the above items were calibrated using a Brooks Vol-u-meter. Model numbers 1052, 1054, 1055, 1057, 1058 at an accuracy of $\pm .2\%$, whose Calibration is traceable to the U.S. National Bureau of Standards.

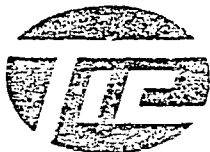
CALIBRATED BY Michael J. Amick
DATE 2-18-87
REMARKS _____

Mass Flowmeter Calibration Worksheet

Byron A. Barnes 2-5-87

UNADJUSTED CALIBRATION						ADJUSTED CALIBRATION					
Parameter Point	1	2	3	4	5	Parameter Point	1	2	3	4	5
Time (sec)	12.6	16.2	23.0	39.3	53.2	Time (sec)					
Time (sec)	12.6	16.3	23.0	39.3	53.1	Time (sec)					
Time (sec)	12.7	16.2	23.0	39.3	53.0	Time (sec)					
Average	12.6	16.2	23.0	39.3	53.1	Average					
Volume (cc)	10	10	10	10	10	Volume (cc)					
Flowrate cc/min	47.62	37.04	26.09	15.27	11.30	Flowrate cc/min					

Best Available Copy



Tampa Instrumentation Center, Inc.

6801 NORTH 54th STREET * TAMPA, FLORIDA 33610

(813) 623-3979

Certificate of Inspection

OWNER OF ITEM Environmental Engineering REPORT NO. 000802

ITEM Digital Multimeter MFR. Simpson

MODEL NO. 463 SERIAL NO. A15560

CALIBRATION DATE 3/12/87 RECALIBRATION DUE 3/12/88

TECHNICIAN JSH PROCEDURE USED Mfg

ENVIRONMENTAL CONDITIONS 72 °F 45 %RH

ITEM FOUND: [X] WITHIN TOLERANCE [] OUT OF TOLERANCE (ADJUSTMENT REQ'D) [] OUT OF TOLERANCE, REPAIR REQ'D [] INOPERATIVE UPON RECEIPT

ITEM RETURNED: [X] WITHIN TOLERANCE [] CORRECTION CHART SUPPLIED

SPECIFICATIONS/REMARKS:

The above listed instrument has been duly tested and inspected and found to meet all published physical and operating specifications.

STANDARDS USED IN THIS CALIBRATION:

Table with 6 columns: MFR., MODEL, SERIAL NO., DATE CAL., DUE, REMARKS. Row 1: Fluke, 760, TIC-011, 2/2/87, 2/2/88.

The accuracy of the listed above standards used in performing the calibration were periodically compared to directly, or indirectly with a National Standard or accuracy was derived thru ratio self-calibration techniques.

INSP. TIC 42 BY Jim Hunkle

CALIBRATED AT LABORATORY [X] IN PLANT []

Environmental Engineering Consultants, Inc.

~~Recorder Calibration~~

DVM

~~Site~~

~~Parameter~~

CALIBRATED AGAINST: Recorder: Manufacturer <u>SIMPSON</u> Model No. <u>463</u> Serial No. <u>A15560</u> CALIB. DATE <u>3/12/87</u>		VOLTAGE 0.000 0.007		RECORDER READING		
Digital Multimeter: Manufacturer <u>NLS</u> Model No. <u>PM 450</u> Serial No. <u>193261</u> Calibration Date <u>3/30/87</u>		Test Point SIMPSON Unadjusted	NLS Adjusted	% Chart Unadjusted	% Chart Adjusted	
		1	0.502	0.495		
		2	1.000	0.993		
		3	3.00	3.007		
		4	3.99	3.999		
		5	4.99	4.998		
		6	6.00	6.005		
		7	6.99	6.998		
		8	8.01	8.018		
		9	9.00	9.016		
		10	10.01	10.020		

Voltage Source:

Manufacturer EEC
 Model No. —
 Serial No. —

Calibrated By *[Signature]*
 Date 3/30/87

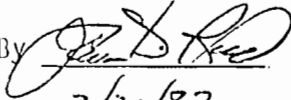
Environmental Engineering Consultants, Inc.

~~Recorder Calibration~~

DVM

~~Site~~ _____

~~Parameter~~ _____

CALIBRATED AGAINST:		VOLTAGE		RECORDER READING	
Recorder:		0.000	0.001		
Manufacturer	<u>SIMPSON</u>	SIMPSON	NLS	% Chart Unadjusted	% Chart Adjusted
Model No.	<u>463</u>	Unadjusted	Adjusted		
Serial No.	<u>A15560</u>				
<small>CALIB.</small> Range-DATE	<u>3/12/87</u>				
Digital Multimeter:		1	0.502	0.502	
Manufacturer	<u>ALLIANT</u>	2	1.005	1.005	
Model No.	<u>PM 450</u>	3	2.99	2.998	
Serial No.	<u>193260</u>	4	4.00	4.002	
Calibration Date	<u>3/30/87</u>	5	5.01	5.015	
Voltage Source:		6	6.00	6.002	
Manufacturer	<u>EEC</u>	7	7.01	7.015	
Model No.	<u>—</u>	8	7.99	7.995	
Serial No.	<u>—</u>	9	9.00	9.002	
Calibrated By		10	10.01	10.008	
Date	<u>3/30/87</u>				

APPENDIX D
PROJECT PARTICIPANTS

PROJECT PARTICIPANTS

Carl F. Fink	Team Test Leader Report Preparation Field Testing
Jack Fross	Field Testing
Byron Burrows	Field Testing
James Root	Field Testing
Henry Von Demfange	Ogden Projects, Inc. Observer
Fred Hartledge	Thornton Laboratories, Inc. Supervisor