June 25, 1986

DER IIII 1 1988

BAQM

Mr. Bill Thomas Permits Division Florida Department of Environmental Regulation 2200 Blair Stone Road Tallahassee, Florida 32301

Dear Mr. Thomas:

This will serve to transmit copies of General Portland's request for a modification to Construction Permit No. AC29-094093 dated February 5, 1985. General Portland requests approval to construct a vacuum type cement unloading system at our plant in Tampa, Florida. We have, in the past several months, discussed this project with you, Mr. Claire Fancy, Mr Dan Williams and Mr. Roger Stewart and his staff of the Hillsborough County Environmental Protection Commission. The permit modification request has been completed following your suggestions and is submitted for your review and approval.

General Portland intends to purchase two vacuum type ship unloading systems each rated at 400 tons per hour and install them on our dock on Sparkman Channel in the Port of Tampa.

The cement will be placed on an existing conveyor belt using Dust collection installed in the Phase I Clinker Project and conveyed to a new 30,000 ton cement storage silo. Transfer points will be controlled with existing Dust Collectors. A large portion of the total 900,000 tons per year will be loaded from the silo directly into bulk cement tanker trucks for customer delivery. A smaller tonnage will be reground in existing finish mills to produce masonry and other specialty cements. The unloading, conveying, storage and loadout facilities will be dust free utilizing high efficiency pulse jet type dust collectors to insure dust free operation.

General Portland requests continuation of our presently permitted Phase I Clinker Unloading System and replacement of the Phase II clinker construction plan with the vacuum cement unloading system described in this application.

Page 2 Mr. Bill Thomas June 25, 1986

General Portland sincerely appreciates the efforts of the DER and Hillsborough County in the review and permitting of this modification. If at any time you require additional information or I may be of any additional service, please do not hesitate to contact me at 214/934-7100.

Yours truly,

William H. Winders Environmental Manager

WHW:ss Attachments

cc: E. H. Sundquist R. D. Auten

Mr. Roger Stewart

June 25, 1986

Mr. Roger Stewart, Director Hillsborough County Environmental Protection Commission 1900 Ninth Avenue Tampa, Florida 33602

Dear Mr. Stewart:

This will serve to transmit copies of General Portland's request for a modification to Construction Permit No. AC29-094093 dated February 5, 1985. General Portland requests approval to construct a vacuum type cement unloading system at our plant in Tampa, Florida. We have, in the past several months, discussed this project with you and your staff, Mr. Claire Fancy, Mr Dan Williams, and Mr. Bill Thomas of the Florida Department of Environmental Regulation (DER). The permit modification request has been completed following Mr. Thomas' suggestions and is submitted for your review and comments to the Florida Department of Environmental Regulation (DER).

General Portland intends to purchase two vacuum type ship unloading systems each rated at 400 tons per hour and install them on our dock on Sparkman Channel in the Port of Tampa.

The cement will be placed on an existing conveyor belt using Dust collection installed in the Phase I Clinker Project and conveyed to a new 30,000 ton cement storage silo. Transfer points will be controlled with existing and new Dust Collectors. A large portion of the total 900,000 tons per year will be loaded from the silo directly into bulk cement tanker trucks for customer delivery. A smaller tonnage will be reground in existing finish mills to produce masonry and other specialty cements. The unloading, conveying, storage and loadout facilities will be dust free utilizing high efficiency pulse jet type dust collectors to insure dust free operation.

General Portland requests continuation of our presently permitted Phase I Clinker Unloading System and replacement of the Phase II clinker construction plan with the vacuum cement unloading system described in this application.

Page 2 Mr. Roger Stewart June 25, 1986

General Portland Inc. sincerely appreciates the efforts of HCEPC in the review and anticipated support of this modification. Please advise me, as soon as possible, of the correct permit application fees, and we shall remit. If at any time you require additional information, or if I may be of any assistance, please do not hesitate to contact me at (214) 934-7100.

Yours truly,

William H. Winders Environmental Manager

WHW:ss Attachments

cc: E. H. Sundquist R. D. Auten Mr. Bill Thomas

#### STATE OF FLORIDA

#### DEPARTMENT OF ENVIRONMENTAL REGULATION

SOUTHWEST DISTRIC

7601 HIGHWAY 301 NORTH TAMPA, FLORIDA 33610 JUL 1 1986



GOVERNOR

WILLIAM K. HENNESSEY DISTRICT MANAGER

O PERMIT #AC 29-094093 DATED FEB. 5, 1985. APPLICATION TO OPERATE/CONSTRUCT AIR POLLUTION SOURCES

SOURCE TYPE: PORTLAND CEMENT PLANT [] New1 [X] Existing1
SOURCE TYPE: PORTLAND CEMENT PLANT [] New1 [X] Existing1  APPLICATION TYPE: [] Construction [] Operation [X] Modification
COMPANY NAME: GENERAL PORTLAND INC. COUNTY: Hillsborough
Identify the specific emission point source(s) addressed in this application (i.e. Lime Cement Unloading, Kiln No. 4 with Venturi Scrubber; Peaking Unit No. 2, Gas Fired) Transfer & Storage
SOURCE LOCATION: Street 2001 Maritime Blvd. City Tampa
UTM: East 17-358.OE North 3090.7N
D & Latitude 27° 56' 04"N Longitude 82° 26' 44"W
APPLICANT NAME AND TITLE: Eric Sundquist, Vice President & General Manager
APPLICANT ADDRESS: 1111 North West Shore Blvd., Tampa, Fla. 33622

#### SECTION I: STATEMENTS BY APPLICANT AND ENGINEER

#### APPLICANT

I am the undersigned owner or authorized representative\* of GENERAL PORTLAND INC.

I certify that the statements made in this application for a Construction/Modification permit are true, correct and complete to the best of my knowledge and belief. Further, I agree to maintain and operate the pollution control source and pollution control facilities in such a manner as to comply with the provision of Chapter 403, Florida Statutes, and all the rules and regulations of the department and revisions thereof. also understand that a permit, if granted by the department, will be non-transferable and I will promptly notify the department upon sale or legal transfer of the permitted establishment.

\*Attach letter of authorization

War ..

Signed:

Vice-President General Manager Eric H. Sundquist,

Name and Title (Please Type)

Date: 6/26/86 Telephone No.813/872-7777

B. PROFESSIONAL ENGINEER REGISTERED IN FLORIDA (where required by Chapter 471, F.S.)

This is to certify that the engineering features of this pollution control project have been designed/examined by me and found to be in conformity with modern engineering principles applicable to the treatment and disposal of pollutants characterized in the permit application. There is reasonable assurance, in my professional judgment, that

1 See Florida Administrative Code Rule 17-2.100(57) and (104)

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Effective October 31, 1982

Indicate any previous DER permits, orders and notices associated with the emission

See attached Sheet #3 for DER Permits.

point, including permit issuance and expiration dates.

Ε.		
	if power plant, hrs/yr; if seasonal, describe: The import of 900	,000 tons per
	year of cement, will require an average of 33 ships/year and	
	cargo size of 27,300 tons/ship with an average unloading rate average 52 hrs/ship. and average 1733 hr/yr. Each source may and its operating time is listed separately.	of 520 tons/hr., vary slightly
F.	If this is a new source or major modification, answer the following quest (Yes or No)	ions.
	l. Is this source in a non-attainment area for a particular pollutant?	Yes
	a. If yes, has "offset" been applied?	N/A*
	b. If yes, has "Lowest Achievable Emission Rate" been applied?	N/A*
	c. If yes, list non-attainment pollutants.	
	<ol> <li>Does best available control technology (BACT) apply to this source?</li> <li>If yes, see Section VI.</li> </ol>	No
	<ol> <li>Does the State "Prevention of Significant Deterioriation" (PSD) requirement apply to this source? If yes, see Sections VI and VII.</li> </ol>	No
	4. Do "Standards of Performance for New Stationary Sources" (NSPS) apply to this source?	No
	5. Do "National Emission Standards for Hazardous Air Pollutants" (NESHAP) apply to this source?	No
н.	Do "Reasonably Available Control Technology" (RACT) requirements apply to this source?	N/A

b. If yes, in addition to the information required in this form, any information requested in Rule 17-2.650 must be submitted.

a. If yes, for what pollutants?\_\_\_\_\_

Attach all supportive information related to any answer of "Yes". Attach any justification for any answer of "No" that might be considered questionable.

\* N/A per Mr. Bill Thomas DER Tallahassee 8/15/84 and 6/24/86

#### SECTION III: AIR POLLUTION SOURCES & CONTROL DEVICES (Other than Incinerators)

A. Raw Materials and Chemicals Used in your Process, if applicable:

	Contam	inants	Utilization	
Description	Туре	% Wt	Rate - lbs/hr	Relate to Flow Diagram
				See Attachments and
				Drawing.
	·			

В.	Process	Rate.	if	applicable:	(See	Section V	Item :	1)	١

1.	Total Process	Input Rai	te (lbs/hr):_	Varible	up	to	2,000,000 (lbs/hr)

2.	Product	Weight	(lbs/hr):	$\mathtt{Same}$	as	Item	1

C. <u>Airborne Contaminants-Emitted: (Information in this table must be submitted for each emission point, use additional sheets as necessary)</u>

Name of	Emiss	ion <sup>l</sup>	Allowed <sup>2</sup> Emission Rate per	Allowable <sup>3</sup>	Potential <sup>4</sup> Emission	Relate to Flow
Contaminant	Maximum lbs/hr	Actual T/yr	Rule 17-2	lbs/hr	lbs/yr T/yr	Diagram
Particulate			17-2.610(2)	**	See Attached	See 5
	Sheet #V				Sheet #V.	Below
Fugitive Pa	rticulate		17-2.610(3)			_
					·	

<sup>15</sup>ee Section V, Item 2. \*(See Attached Sheet "Emission Calculations")

<sup>&</sup>lt;sup>2</sup>Reference applicable emission standards and units (e.g. Rule 17-2.600(5)(b)2. Table II, E. (1) - 0.1 pounds per million BTU heat input)

<sup>&</sup>lt;sup>3</sup>Calculated from operating rate and applicable standard. See Attached Emission Calculations

 $<sup>^{4}</sup>$ Emission, if source operated without control (See Section V, Item 3).

<sup>\*\*</sup>  $48,560 \times .03 \times 1/7000 \times 60 = 12.48 \#/hr$ .

D. Control Devices: (See Section V, Item 4)

Name and Type (Model & Serial No.)	Contaminant	Efficiency	Range of Particles Size Collected (in microns) (If applicable)	Basis for Efficiency (Section V Item 5)	
Industrial Filter	Particulate	99.9%	<del>_</del>	Purchase	
Fabric Filters, or	equal.			Specificat: Sheets Att	ons ched
See Attached Sheets	5				
				Attachmen	t VI

#### E. Fuels

	Consump	tion*	
Type (Be Specific)	avq/hr	max./hr	Maximum Heat Input (MMBTU/hr)
N/A			·
<del></del>			
	·		· · · · · · · · · · · · · · · · · · ·
	i i	Į	

\*Units: Natural Gas--MMCF/hr; Fuel Oils--gallons/hr; Coal, wood, refuse, other--lbs/hr.

F		1	A	n o	1	v		i	•	
г	uв	1	_	на		7	3	_	3	•

Percent Sulfur:		Percent Ash:	<del></del>
Density:	lbs/gal	Typical Percent Nitrogen:	
Heat Capacity:	BTU/16		BTU/gal
Other Fuel Contaminants (which	ı may cause air p	ollution):	
F. If applicable, indicate th	e percent of fue	l used for space heating.	
Annual Average	Ma	ximum	
Annual Average  G. Indicate liquid or solid w			

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	ht:	*			ft.	Sta	ck Diamete	r:*	f
as Flow R	ate:	*	ACFM	*	_DSCFM	Gas	Exit Temp	erature:	*
ater Vapo	r Content	: _			%	Vel	ocity:	*	FI
To be sı	applied	wit	h Operat SECT				cation INFORMATI	ON .	
Type of Waste			Type I (Rubbish)						Type VI (Solid By-prod.
Actual lb/hr Inciner- ated									
Uncon- trolled lbs/hr)				,					
			<b></b>		<del></del>				····
tal Weigl	nt Incine e Number	rate	Hours of (	r) Operation	per da	у			
otal Weigl oproximat anufactur	nt Incine e Number er	rate of i	ed (lbs/hi	r)	per da	у	day/	wk	hr)wks/yr
tal Weigl proximat	nt Incine e Number er	rate	ed (lbs/hi	r)	per da	lel N	day/	wk	wks/yr
tal Weigl proximat nufactur ite Const	nt Incine e Number er ructed	rate	ed (lbs/hi	r)  Operation  Heat R	per da	lel N	day/	wk	wks/yr
tal Weigl proximat nufactur te Const	nt Incine e Number er ructed	rate	ed (lbs/hi	r)  Operation  Heat R	per da	lel N	day/	wk	wks/yr
tal Weigl proximat nufactur te Const  rimary Cl	nt Incine e Number er ructed hamber	rate	ed (lbs/hi	T)  Deration  Heat R  (BTU	per da Mod elease /hr)	le1 N	day/	BTU/hr	wks/yr
tal Weigl proximat nufactur te Const  rimary Cl econdary ack Heigl	nt Incine e Number er ructed hamber Chamber	rate	ed (lbs/hi Hours of (  Volume (ft) <sup>3</sup>	Heat R (BTU	per daMod elease /hr)	le1 N	day/	BTU/hrStack T	Temperature (°F)
rimary Clecondary ack Heights Flow Ref	nt Incine e Number er ructed Chamber ht:	pe:	Volume (ft)	Heat R (BTU	per daMod elease /hr)	lel N	day/	BTU/hr  Stack T	Temperature (°F)

ltimate disp	osal of	any ef	fluent	other	than	that	emitted	from	the	stack	(acrubber	water
--------------	---------	--------	--------	-------	------	------	---------	------	-----	-------	-----------	-------

NOTE: Items 2, 3, 4, 6, 7, 8, and 10 in Section V must be included where applicable.

#### SECTION V: SUPPLEMENTAL REQUIREMENTS

Please provide the following supplements where required for this application.

- 1. Total process input rate and product weight -- show derivation [Rule 17-2.100(127)]
- To a construction application, attach basis of emission estimate (e.g., design calculations, design drawings, pertinent manufacturer's test data, etc.) and attach proposed methods (e.g., FR Part 60 Methods 1, 2, 3, 4, 5) to show proof of compliance with applicable standards. To an operation application, attach test results or methods used to show proof of compliance. Information provided when applying for an operation permit from a construction permit shall be indicative of the time at which the test was made.
- 3. Attach basis of potential discharge (e.g., emission factor, that is, AP42 test).
- 4. With construction permit application, include design details for all air pollution control systems (e.g., for baghouse include cloth to air ratio; for scrubber include cross-section sketch, design pressure drop, etc.)
- 5. With construction permit application, attach derivation of control device(s) efficiency. Include test or design data. Items 2, 3 and 5 should be consistent: actual emissions = potential (1-efficiency).
- 6. An 8 1/2" x 11" flow diagram which will, without revealing trade secrets, identify the individual operations and/or processes. Indicate where raw materials enter, where solid and liquid waste exit, where gaseous emissions and/or airborne particles are evolved and where finished products are obtained.
- 7. An 8 1/2" x 11" plot plan showing the location of the establishment, and points of air-borne emissions, in relation to the surrounding area, residences and other permanent structures and roadways (Example: Copy of relevant portion of USGS topographic map).
- 8. An 8  $1/2^n \times 11^n$  plot plan of facility showing the location of manufacturing processes and outlets for airborne emissions. Relate all flows to the flow diagram.

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9.	The appropriate	application fee in accordance wi	th Rule 17-4.05.	The check should be
	made payable to	the Department of Environmental	Regulation.	

10. With an application for operation permit, attach a Certificate of Completion of Construction indicating that the source was constructed as shown in the construction permit.

#### SECTION VI: BEST AVAILABLE CONTROL TECHNOLOGY

	SECTION VII BEST AVAILA	IDLE CONTROL TECHNOLOGY
Α.	Are standards of performance for new stat applicable to the source?	ionary sources pursuant to 40 C.F.R. Part 60
	[ ] Yes [X] No	·
	Contaminant	Rate or Concentration
В.		ol technology for this class of sources (If
	[ ] Yes [ X] No	
	Contaminant	Rate or Concentration
c.	What emission levels do you propose as bes	t available control technology?
	Contaminant Particulate Emissions	Rate or Concentration See Attachments
D.	Describe the existing control and treatmen	t technology (if any).
	1 Control Device/Systems	2 Operating Principles.

l. Control Device/System:

Operating Principles:

3. Efficiency:\*

4. Capital Costs:

\*Explain method of determining

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	5.	Useful Life:		6.	Operating Costs:	
	7.	Energy:		8.	Maintenance Cost:	
	9.	Emissions:				
		Contaminant			Rate or Concentration	
				_		
=					<del></del>	
	10.	Stack Parameters				
	a.	Height:	ft.	b.	Diameter:	ft.
	c.	Flow Rate:	ACFM	d.	Temperature:	°F.
	e.	Velocity:	FPS			
Ε.		cribe the control and treatment additional pages if necessary).	techn	olog	y available (As many types as	applicable,
	1.					
	a.	Control Device:		ь.	Operating Principles:	
	c.	Efficiency: 1		d.	Capital Cost:	
	е.	Useful Life:		f.	Operating Cost:	\$F-+
	g.	Energy: 2		h.	Maintenance Cost:	
	i.	Availability of construction ma	terial	s an	d process chemicals:	,
	j.	Applicability to manufacturing	proces	ses:		
	k.	Ability to construct with contr within proposed levels:	ol de	vice	, install in available space,	and operate
	2.					
	а.	Control Device:		b.	Operating Principles:	
	c.	Efficiency: 1		d.	Capital Cost:	
	e.	Useful Life:		f.	Operating Cost:	
	g.	Energy: <sup>2</sup>		h.	Maintenance Cost:	
,	i.	Availability of construction may	terial	s an	d process chemicals:	

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Applicability to manufacturing processes: Ability to construct with control device, install in available space, and operate within proposed levels: 3. Control Device: Operating Principles: Efficiency: 1 Capital Cost: Useful Life: Operating Cost: Energy: 2 g. Maintenance Cost: i. Availability of construction materials and process chemicals: Applicability to manufacturing processes: Ability to construct with control device, install in available space, and operate within proposed levels: 4. Control Device: 8. b. Operating Principles: Efficiency: 1 c -Capital Costs: \_Usefu-l\_L-i-f-e:\_ f. Operating Cost: Energy: 2 Maintenance Cost: Availability of construction materials and process chemicals: Applicability to manufacturing processes: j. Ability to construct with control device, install in available space, and operate within proposed levels: Describe the control technology selected: Control Device: Fabric Filters ı. 2. Efficiency: 1 99.9% 3. Capital Cost: Useful Life: Not Available \$286,000 4. Operating Cost: Unknown Energy: 2 6. Not Available Manufacturer: Industrial Filter & Equal 7. Maintenance Cost: Unknown 8. Other locations where employed on similar processes: (1) Company: GENERAL PORTLAND INC. (2) Mailing Address: (3) City:

 $^{
m l}$ Explain method of determining efficiency. <sup>2</sup>Energy to be reported in units of electrical power - KWH design rate.

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F.

(4) State:

(5) Environmental Manag	ger: William H.	Winders		
(6) Telephone No.:	(214) 934-	7148		
(7) Emissions: 1				
Conteminant	Ė		Rate or Conce	entration
			-	
(8) Process Rate: 1				
b. (1) Company:				
(2) Mailing Address:				
(3) City:		(4) State:		
(5) Environmental Manag	jer:			
(6) Telephone No.:				
(7) Emissions: 1				
Contaminant	:		Rate or Conce	entration
				•
(8) Process Rate: 1				
10. Reason for selection	n and description	of systems:		
Applicant must provide thi available, applicant must s			Should this	s information not b
SECTION V	II - PREVENTION O	F SIGNIFICANT	DETERIORATIO	IN .
A. Company Monitored Data				
1no. sites	TSP _	. ()	502+	Wind spd/dir
Period of Monitoring	month d	/ to	month day	/ year
Other data recorded				
Attach all data or stati	stical summaries	to this applic	cation.	
*Specify bubbler (B) or cont	inuous (C).			
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	a. Was instrument	tation EPA re	ferenced or its e	quivalent?	[ ] Yes	[ ] No	•
	b. Was instrument	tation calibr	ated in accordance	e with Depa	rtment p	cocedure	s?
	[ ] Yes [ ] !	lo [] Unkno	wn				
в.	Meteorological Da	a Used for A	ir Quality Modeli	n g			
	1 Year(s)	of data from	month day year	to /	day year	<b>.</b>	
	2. Surface data	obtained from	(location)	<u>.</u>	·		
	3. Upper air (mi	king height)	data obtained fro	m (location	)		
	4. Stability win	d rose (STAR)	data obtained fr	om (locatio	in)		
c.	Computer Models U	sed					
	1.	<del></del>		Modified?	If yes,	attach	description.
	2.	<u></u>		Modified?	If yes,	attach	description.
	3.			Modified?	If yes,	attach	description.
	4,-			Modified?	If yes,	attach	description.
	Attach copies of ciple output table		el runs showing i	nput data,	receptor	locatio	ins, and prin-
D.	Applicants Maximus	n Allowable E	mission Data				
	Pollutant	Ε	mission Rate				
	TSP			gra	ms/sec		
	so <sup>2</sup>			gre	ms/sec	-	
Ε.	Emission Data Use	d in Modeling					
	Attach list of em	ission source	s. Emission data	required i	S SOUICE	name, c	description of

F. Attach all other information supportive to the PSD review.

2. Instrumentation, Field and Laboratory

G. Discuss the social and economic impact of the selected technology versus other applicable technologies (i.e., jobs, payroll, production, taxes, energy, etc.). Include assessment of the environmental impact of the sources.

point source (on NEDS point number), UTM coordinates, stack data, allowable emissions,

H. Attach scientific, engineering, and technical material, reports, publications, journals, and other competent relevant information describing the theory and application of the requested best available control technology.

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and normal operating time.

### PROJECT MODIFICATION EMISSION SUMMARY

Dust Collector No.	Emissions Tons Per Year	
(27)	2.34 ~ 1	
28)	0.78 7	3 4 5
42)	4.14 7	3,12
43)	4.01 ↓	
<u>(44)</u> _	1.18 7	
45)	1.18 1	
46	0.09	
47	0.09	ţ.
48	0.30	
49	0.82	
(50)	<del></del>	?

Total Project Emissions

\_ 14.93

X

### CLINKER PROJECT PHASE I AS BUILT EMISSIONS SUMMARY

,		
Dust Collector		
No. 26		
10,000 X .03	X 1/7000 X 60 X 1/2000 X 1600	= 2.06
✓ No. 27_		
18,000 X .03 X	X 1/7000 X 60 X 1/2000 X 1600	= 3.70 . / 6 )
√ No. 28		
6,000 X .03 >	X 1/7000 X 60 X 1/2000 X 1600	= 1.23
	Total Emissions Tons/Year	= 6.99
1982 = 83 =	86 = )25	PX/ TPY-
84- 85= -186=1-7		MSR.
= 625TPL non-all NOR-F	Attramentare :-	
,		777
with the same of t	1986-15779 increase -+ newconsti	
meslace 8.00	, · en imail	total energe

### DESCRIPTION OF THE PROPOSED MODIFICATION TO THE TAMPA CLINKER UNLOADING PROJECT PHASE II AND REPLACEMENT WITH A FINISHED CEMENT UNLOADING SYSTEM FOR THE TAMPA PLANT

This permit modification is intended to cancel Phase II of the Cement Clinker Unloading Project, authorized in Construction Permit No. AC29-094093 dated February 5, 1985; and replace it with the construction of a vacuum-type ship unloading system. The vacuum-type system is an environmentally secure system and clearly superior to other open-hold unloading equipment presently available.

General Portland Inc. seeks construction permit authority for a vacuum finished cement unloading system to unload 900,000 tons per year of Portland Cement from gearless bulk cargo ships and to continue the unloading of cement clinker at our dock through the presently permitted Phase I clinker unloading system as built. Permission is not requested for both operations concurrently, except during the period of construction and transition from clinker to cement. During this period we do not intend to import more product than approved. At the completion of construction of the vacuum cement unloading system General Portland intends to seek an operating permit which will allow the unloading of finished cement.

finished cement unloading project includes the General Portland's construction of a new concrete dock section, three new dolphins, and a new shore mooring at the northwest corner of our property (separate permits will be submitted for this dock work). The purchase of two vacuum type 400 ton per hour ship unloading systems as manufactured by Cyclonaire or their equal will provide a dust-free environmentally sound ship unloading system. We will utilize the present existing and permitted Dust Collector No. 27 and 28 in the transfer of the cement over the existing No. 7 conveyor belt. We will construct a new 30,000 ton storage silo and install Dust Collector No. 43 to vent the silo during loading. A new Dust Collector No. 42, will vent the air slides and the bulk cement truck loading spouts under the large storage silo. Four new small Dust Collectors will be added to vent cement transport for regrinding. The Cyclonaire vacuum systems also have internal dust control systems which are highly efficient.

This application as submitted is intended to include all particulate and fugitive particulate emissions sources in the categories of cement unloading, transport, handling, storage and loadout of the Cement Unloading System at the Tampa Plant.

Drawings attached to this request for modification cover:

 the process flow of presently existing and permitted equipment;

- (2) a layout of the Phase I Clinker Unloading Project as built, and the Phase II Clinker Unloading Project which is hereby abandoned;
- (3) the flow schematic and layout of the proposed equipment associated with the cement vacuum unloading, transport and storage system.

### COSTS OF POLLUTION CONTROL SYSTEMS TAMPA CEMENT UNLOADING, HANDLING AND STORAGE

Location & Item	Purchase	Installation	<u>Total</u>
30,000 Ton Storage Silo Top, 1–1800 CFM Baghouse with Fan and Ductwork	60,000	20,000	80,000
30,000 Ton Storage Silo- Bottom, 1-8000 CFM Bag- house with Fan and Duct Work	25,000	15,000	40,000
Mill Feed Silos-Bottom 4–1500 CFM Insertable Dust Filters with Fans	16,000	9,000	25,000
Compressor	7,000	10,000	17,000
Power and Wiring	18,000	46,000	64,000
Sub Total	126,000	100,000	226,000
Engineering		34,000	34,000
Contingency	13,000	13,000	26,000
	<del></del>		
TOTAL	139,000	147,000	286,000

### GENERAL PORTLAND INC. TAMPA PLANT

#### OUTSTANDING DER OPERATING PERMITS

DER Number	Source	Expiration Date
A029-51703	Kiln #6	April, 1987
A029-51704	#6 Clinker Cooler	April, 1987
A029-47658	#6 Precip Dust	January, 1987
	Handling	• •
A029-47651	Stor/Load White (III)	January, 1987
A029-47652	Bulk Cem Stor Load	January, 1987
A029-47653	Mat. Handling	January, 1987
AO29-47654	Finish Mills	January, 1987
A029-47655	Stor/Load, Grat	January, 1987
	(III)	
A029-47656	Cement Stor/Pkg	January, 1987
A029-47657	Truck-Track Scale	January, 1987
A029-47659	Finish Grind	January, 1987
	Storage	• •
AO29-55964	Finish Mill DC	July, 1987
	8c & 10c	,
AO29-47661	White Cem Stor/	January, 1987
	Pkg	, = :
A029-47662	Mason Cem Stor/	January, 1987
	Pkg	<b> y ,</b> ·
AO29-56064	Masonry Dust Collector	July, 1987

In addition, FAC, 17-2.650 (2)(c) l.c.(ii) contains a specific Alternate Emission Limitation for General Portland Inc.'s, Tampa plant.

#### PERMIT #AC29-094093 PROPOSED MODIFICATION FOR CEMENT UNLOADING

#### DUST COLLECTOR EMISSION CALCULATIONS:

#### Assumptions:

- 1. Average yearly cement imported 900,000 tons.
- 2. Average ship cargo size of 27,300 tons.
- Average number of ship arrivals is 33 per year.
- 4. Average cement unloading rate is 520 tons/hour including ship movements and clean-up time.
- Average unloading time is 1,733 hrs per year.

#### SAMPLE CALCULATION

18,000 CFM X 0.03 gr/ft<sup>3</sup> X 1/7000 gr/# X 60 min/hr X 1013 hr/yr X 1/2000 #/ton = 2.34 Tons Per Year.

#### Dust Collector No. 27

Collector No. 27 is permitted for 720 hrs/yr by Permit #A029-115401. From Assumptions above, 1733 hours of operation per year will be required. Therefore, (1733 - 720 = (1013)) hrs per year) must be permitted by this modification:

Dust Collector No. 28

Permitted for 720 hrs/yr at 6000 CFM by Permit No. A029-115402 and old location No. 20 is permitted in A029-47653 for 8760 hrs/yr at 6000 CFM. Therefore, the new portion of Dust Collector No. 28 will require (1733 -720 = 1013 hrs/yr) at 6000 CFM.

 $6000 \times .03 \times 1/7000 \times 60 \times 1/2000 \times 1013 = 0.78 \text{ TPY.}$ 

18,000  $\times$  .03  $\times$  1/7000  $\times$  60  $\times$  1/2000  $\times$  1013 =

#### Dust Collector No. 42

Required for bulk cement truck loadout for 16 hrs/day, 5 day/week, 52 wk/yr. less 8 holidays of 16 hrs each or (4160 hr - 128 hr = 4032)hrs/yr).

8000 X .03 X 1/7000 X 60 X 1/2000 X 4032 = 4.14 TPY.

#### Dust Collector No. 43

Requires 1733 hrs/yr from Assumptions above.

18,000 X .03 X 1/7000 X 60 X 1/2000 X 1733 = 4.01 TPY.

#### Dust Collector No. 44

Furnished by Manufacturers of Vacuum Unloading System and guaranteed to meet 0.02 grains per standard cubic foot per minute. 1733 hrs/yr will be required from Assumptions above. Manufacturers information indicates that Dust Collector No. 44 and No. 45 will meet or exceed 0.009 grains per cubic foot of air. The 0.03  $\rm gr/ft^3$  is used for calculation of emissions.

5280 X .03 X 1/7000 X 60 X 1/2000 X 1733 = 1.18 TPY.

#### Dust Collector No. 45

Same rational as Dust Collector No. 44 above.

5280 X .03 X 1/7000 X 60 X 1/2000 X 1733 = 1.18 TPY.

#### Dust Collector No. 46

Support of regrind of Cement in finish mills no. 8, 9 and 10 will require operation for 480 hrs/yr.

1500 X .03 X 1/7000 X 60 X 1/2000 X 480 = 0.09 TPY.

#### Dust Collector No. 47

Support of regrind of Cement in finish Mill No. 8 will require operation for 480 hrs.

1500 X .03 X 1/7000 X 60 X 1/2000 X 480 = 0.09 TPY

#### Dust Collector No. 48

Support of regrind of Cement in finish Mill No. 9 will require operation for 1560 hr/yr.

1500 X .03 X 1/7000 X 60 X 1/2000 X 1560 = 0.30 TPY.

#### Dust Collector No. 49

Support of regrind of Cement in finish Mill No. 10 will require operation for 4281 hrs/yr.

1500 X .03 X 1/7000 X 60 X 1/2000 X 4281 = 0.82 TPY.

Point Number (from Flow D	iagram)		Manufacture	Manufacturer & Model No. (if available)			
Location No. 42			Industrial Filter Model AA-1015 or Equ  Type of Particulate Controlled				
Name of Abatement Device							
Dust Collector			Portland Ce		•		
	GA	SSTREAM	CHARACTERISTICS				
Flow Rate (acfm)		G	as Stream perature ( <sup>0</sup> F)	Particula	te Grain Loading ain/scf)		
Design Maximum Average Ex	pected			Inlet	Outlet		
8,000 8,000	)	Ambie	ent	8	0.02		
Pressure Drop (in. H <sub>2</sub> O)		Water Vapor Content of Effluent Stream (lb water/lb dry air)		(hp)	Requirements (ft <sup>3</sup> /min)		
8		Ambie		30	8,000		
	P		ATE DISTRIBUTION By Weight)				
Micron Range		Inlet		O	Outlet		
0.0-0.5			%		%		
0.5-1.0			%		%		
1.0-5.0		%		<u>.</u>	%		
5-10				%			
10-20			%		%		
over 20		%		%			
		FILTER CH	IARACTERISTICS				
	Diameter (in.)	Bag Leng (ft) 8	th Number of E	- 1	f Compartments aghouse e		
Bag rows will be:			Walkways will	be provided between	banks of bags:		
Staggered - (	Straight )	}	Ye	es (	No )		
Filtering Material: Poly	ester	1					
Describe Bag Cleaning Metho Adjustable Cycle.	d and Cycle:	Rever	se Pulse Jets	of High Pres	ssure Air with		
		ADDITION	IAL INFORMATION				

Point Number (f	rom Flow Diagram)		Manufacturer & Model No. (if available)			
Location No	o. 43		Industrial F	iler Model A	A-1517 or Equal	
Name of Abateme	ent Device		Type of Part	iculate Controlled		
Dust Collec	etor		Portland Ce	ment Dust		
	G.	AS STREAM	CHARACTERISTICS			
Flow Ra	ite (acfm)		erature ( <sup>O</sup> F)		e Grain Loading ain/scf)	
Design Maximum	Average Expected			Inlet	Outlet	
18,000	18,000	Aı	mbient	8	0.02	
Pressur (in.	H <sub>2</sub> O)	of Ei (lb wa	Vapor Content  Iffluent Stream  ater/lb dry air)  mbient	Fan R (hp) 45	equirements (ft <sup>3</sup> /min) 18,000	
			TE DISTRIBUTION Weight)			
Micron	Range	Inlet		Outlet		
0.0-0	).5	i	<b>%</b>		%	
0.5-	1.0	%			%	
1.0-5	5.0		%	<del></del>	%	
5-1			%		%	
10-2			%		<u> </u>	
Over	20		%	. <u></u>	<b>%</b>	
·····	·	<del></del>	ARACTERISTICS			
Filtering Velocity (acfm/ft <sup>2</sup> of Cloth 5.7		Bag Lengt. (ft) 10	h Number of B	in Ba	Compartments ghouse 10	
Bag rows will be:			Walkways will t	oe provided between l	panks of bags:	
Staggered	(Straight)		Yes	5 (	No )	
Filtering Materia	i: Polyester					
Describe Bag Cle Adjustable	aning Method and Cycle: Cycle.	Revers	se Plse Jets (	of High Press	sure Air with	
		ADDITIONA	AL INFORMATION			

Point Number (fr	om Flow Diagram)		Manufacturer & Model No. (if available)				
Location N	0. 46		DCE VOKES Model DLM - VZO/10F				
Name of Abateme	nt Device	<u>-</u>	Type of Particulate Controlled				
Dust Colle	ctor		Portland Ce	ement Dust			
	G	AS STREAM C	HARACTERISTICS	3			
Flow Ra	te (acfm)	Gas Stream Temperature ( <sup>O</sup> F)		Particulate Grain Loading (grain/scf)			
Design Maximum	Average Expected			Inlet	Outlet		
1,500	1,500	Am	nbient	8	0.02		
Pressure (in. I	Prop F <sub>2</sub> O)	Water Vapor Content of Effluent Stream (lb water/lb dry air)		Fan Requirements (hp) (ft <sup>3</sup> /min)			
8		Am	bient	$5\frac{1}{2}$	2,000		
			TE DISTRIBUTION Weight)				
Micron Range		Inlet		Outlet			
0.0-0.5		%			%		
0.5-1	.0	%			%		
1.0-5		% % % % FILTER CHARACTERISTICS		<b>%</b>			
5-10					%		
10-20				<u>%</u>			
over 2	20				%		
	· T = -	<del></del>	<del></del>		• •		
Filtering Velocity (acfm/ft <sup>2</sup> of Cloth) 9.5	Bag Diameter (in.) N/A	Bag Length (ft) N/A	Number of I	•	f Compartments aghouse		
Bag rows will be:				be provided between			
Staggered	( Straight )		Ye	es (	No )		
Filtering Material	Polyester						
<b>Describe Bag Clea</b> Adjustable	ning Method and Cycle: Cycle.	Reverse	Pulse Jets	of High Press	sure Air with		
		ADDITION	LINEODIAMON				
<del></del>		AUDITIONA	L INFORMATION				

Location	om Flow Diagram) No. 47		Manufacturer & Model No. (if available)  DCE VOKES Model DLM - VZO/10F				
Name of Abateme	nt Device		Type of Parti	culate Controlled			
Dust Col	lector		Portland Cen	ment Dust			
	G	AS STREAM (	CHARACTERISTICS				
Flow Rat	te (acfm)	Gas Stream Temperature ( <sup>0</sup> F)			Particulate Grain Loading (grain/scf)		
Design Maximum	Average Expected			Inlet	Outlet		
1,500	1,500	Ambient		8	0.02		
Pressure (in. F	Prop F <sub>2</sub> O)	of Ef	Vapor Content fluent Stream ter/lb dry air)	Fan R (hp)	lequirements (ft <sup>3</sup> /min)		
8		Am	bient	5 <del>1</del> /2	2,000		
	, .		TE DISTRIBUTION Weight)				
Micron I	Range	Inlet		0	Outlet		
0.0-0.5		%			%		
0.5-1.0		%			%		
1.0-5.	<del></del>	% %			<b>%</b>		
5-10				% %			
10-20	<del></del>		%	<del></del>			
over 2	2 <b>0</b>	% FILTER CHARACTERISTICS		%			
****							
Filtering Velocity acfm/ft <sup>2</sup> of Cloth) 9.5		Bag Length (ft) N/A	Number of Ba	• 1	Compartments ghouse ie		
Bag rows will be:			Walkways will be	e provided between l	banks of bags:		
Staggered	· (Straight)		Yes	(	( No )		
Filtering Material  Describe Bag Clea	ning Method and Cycle:		verse Pulse J	ets of High	Pressure Air		
	with Adjustat	ole Cacle	•		<u> </u>		
·		ADDITIONA	L INFORMATION				

Expected	Gas	Type of Partic		e Grain Loading in/scf)	
G/ Expected	Gas	Type of Partic Portland HARACTERISTICS Stream	culate Controlled Cement Dust Particulate (gra	e Grain Loading in/scf)	
G. Expected	Gas	HARACTERISTICS Stream	Particulate (gra	in/scf)	
Expected	Gas	Stream	(gra	in/scf)	
Expected	1		(gra	in/scf)	
•			Inlet		
		1		Outlet	
0	Amt	pient	88	0.02	
	of Eff	luent Stream	Fan Requirements (hp) (ft <sup>3</sup> /min)		
				2,000	
	Inlet		Outlet		
0.0-0.5		%		%	
0.5-1.0		%		%	
	% %		% ··· % % %		
<del></del>		<del></del>	<del></del>		
Sag Diameter (in.) N/A	Bag Length (ft) N/A	Number of Base 20	in Ba	Number of Compartments in Baghouse One	
		Walkways will be	provided between b	anks of bags:	
	I	: Walkways was ov	F	- 3-	
	Bag Diameter	of Eff (lb wat Amb PARTICULAT (By In FILTER CHA Bag Diameter Bag Length	%   %   %     %       %	Of Effluent Stream	

Point Number (from	m Flow Diagram)		Manufacturer & Model No. (if available)			
Location	No. 49		DCE VOKES Model DLM - VZO/10F			
Name of Abatement	t Device		Type of Particulate Controlled			
Dust Col	lector		Portland	Cement Dust		
	G	AS STREAM C	HARACTERISTIC			
Flow Rate	(acfm)	Gas Stream Temperature ( <sup>O</sup> F)		Particulate Grain Loading (grain/scf)		
Design Maximum A	verage Expected	-		Inlet	Outlet	
1,500	1,500	Am	bient	8	0.02	
Pressure I (in. H <sub>2</sub>	•	Water Vapor Content of Effluent Stream (lb water/lb dry air) Ambient		Fan R (hp) 5½	equirements (ft <sup>3</sup> /min) 2,000	
			E DISTRIBUTION Weight)	<del></del>		
Micron Range			Inlet		Outlet	
0.0-0.5		%			%	
0.5-1.0	)	%			<u></u>	
1.0-5.0	<u> </u>		%		<u>%</u>	
5-10		%		· ·	<b>%</b>	
10-20		%			<b>%</b>	
over 20	) 		%		<b>%</b>	
Filtering Velocity (acfm/ft <sup>2</sup> of Cloth) 9.5	Filtering Velocity  Bag Diameter  Bag Lengt  acfm/ft <sup>2</sup> of Cloth)  (in.)  (ft)		Number of 20	in Ba	Number of Compartments in Baghouse One	
Bag rows will be:			Walkways will	be provided between b	oanks of bags:	
Staggered	(Straight)		Y	es (	No )	
Filtering Material:	Polyester					
<del>-</del>	ing Method and Cycle: with Adjustab	Rev le Cycle.	erse Pulse	Jets of High	Pressure Air	
		100				
		ADDITIONA	L INFORMATION			

Point Number (from Flow Diagram)  Location No. 44				Manufacturer & Model No. (if available)				
Name of Abatement Device				Type of Particulate Controlled				
			AS STREAM	и CH	ARACTERISTICS			
Flow Rat	te (acf			Gas Stream Temperature ( <sup>O</sup> F)			Particulate Grain Loading (grain/scf)	
Design Maximum	Avera	ge Expected					Inlet	Outlet
Pressure Drop (in. H <sub>2</sub> O)		Water Vapor Content of Effluent Stream (lb water/lb dry air)			Fan Requirements (hp) (ft <sup>3</sup> /min)			
				ATE By We	DISTRIBUTION eight)			
Micron F	Range			Inle	et		Ou	tlet
0.0-0.	.5				%			%
0.5-1.					%			%
1.0-5.	.0				%			%
5-10	,				%			%
10-20	<u> </u>				%			%
over 2	20		%				%	
			FILTER C	HAR	ACTERISTICS			
Filtering Velocity (acfm/ft <sup>2</sup> of Cloth)		Bag Diameter (in.)	Bag Leng (ft)	gth	Number of Ba	ags	Number of Compartments in Baghouse	
Bag rows will be:			<u></u>		Walkways will b	e prov	ided between ba	anks of bags:
Staggered	-	Straight		Walkways		<b>.</b>	No	
Filtering Material:	:							
Describe Bag Clea	ning N	Method and Cycle:				<u></u>		
		<del></del>	ADDITIO	NAT	INFORMATION			<del></del>

Information considered proprietary by manufacturer of Vacuum Unloading System and not available at this time.

Point Number (from Flow Diagram) Location No. 45				Manufacturer & Model No. (if available)			
Name of Abatement Device				Type of Particulate Controlled			
		GAS STREAM	 Λ CH.	RACTERISTICS		···	
Flow Rate (		T	Gas Stream Temperature ( <sup>O</sup> F)		Particulate Grain Loading (grain/scf)		
Design Maximum Av	erage Expected				Inlet	Outlet	
Pressure D	Water Vapor Content of Effluent Stream (lb water/lb dry air)		ent Stream	Fan Requirements (hp) (ft <sup>3</sup> /min)			
			ATE : By We	DISTRIBUTION ight)		*	
Micron Rar	Inlet			Outlet			
0.0-0.5	0.0-0.5			%	%		
0.5-1.0	<del>-</del>	%		%			
1.0-5.0		% % % %			% - · %		
5-10	_			%			
10-20				%	% %		
over 20				%			
		FILTER C	HARA	CTERISTICS			
Filtering Velocity (acfm/ft <sup>2</sup> of Cloth)	Bag Diameter (in.)	Bag Leng (ft)	<b>zth</b>	Number of Bags	Number of Compartments in Baghouse		
Bag rows will be:		· <u>·</u>	,	Walkways will be pr	ovided between b	anks of bags:	
Staggered	Straight		Yes		No		
Filtering Material:							
Describe Bag Cleanin	g Method and Cycle:						
						<u>,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,</u>	
		ADDITION	NAL I	NFORMATION			

Information considered proprietary by manufacturer of Vacuum Unloading System and not available at this time.

ATTACHMENT VII

DATE: May 13, 1986

GENERAL PORTLAND DALLAS, TEXAS

ATTN: Mr. William H. Winders

FROM: Fred Wuertele

RE: Air quality specifications for Docksider KV-Tampa

This is the air quality information for each of the 400 TPH units proposed for the Tampa facility:

- 1. Filter Area: Each vacuum kettle has an approximate filter area of 2,200 square feet.
- 2. Vacuum pump discharge volume: Each system is equipped with three vacuum pumps which are identical. The total volume of air discharged varies depending on the operating conditions. The rated inlet volume (three units together) is 13,200 ICFM at 18 inches Eg. Thus while the unit is in operation the air discharged from the vacuum pumps is 5,280 ACFM. While the unit is idling with the vacuum pump running, the amount of sir discharged will be approximately 17,000 ACFM.
- 3. Particulate matter discharged from vacuum pumps:
  - a. While the unit is operating at optimum capacity approximately 0.57 milligrams of dust will be contained in every cubic foot of air discharged. This means that 3,010 milligrams per minute of dust will be discharged from the system exhaust.
  - b. While the unit is idling with the vacuum pump running, I estimate that the amount of particulate material discharged will be reduced to approximately 10% or 0.057 milligrams of dust per cubic foot of air discharged. This will be approximately 969 milligrams per minute of dust discharged from each system exhaust.

As you can see from above the worst case for the particulate matter discharge will be the former, however, while the unit is idling a much greater amount of air will be discharged. Please feel free to call on me directly if you require any additional information.

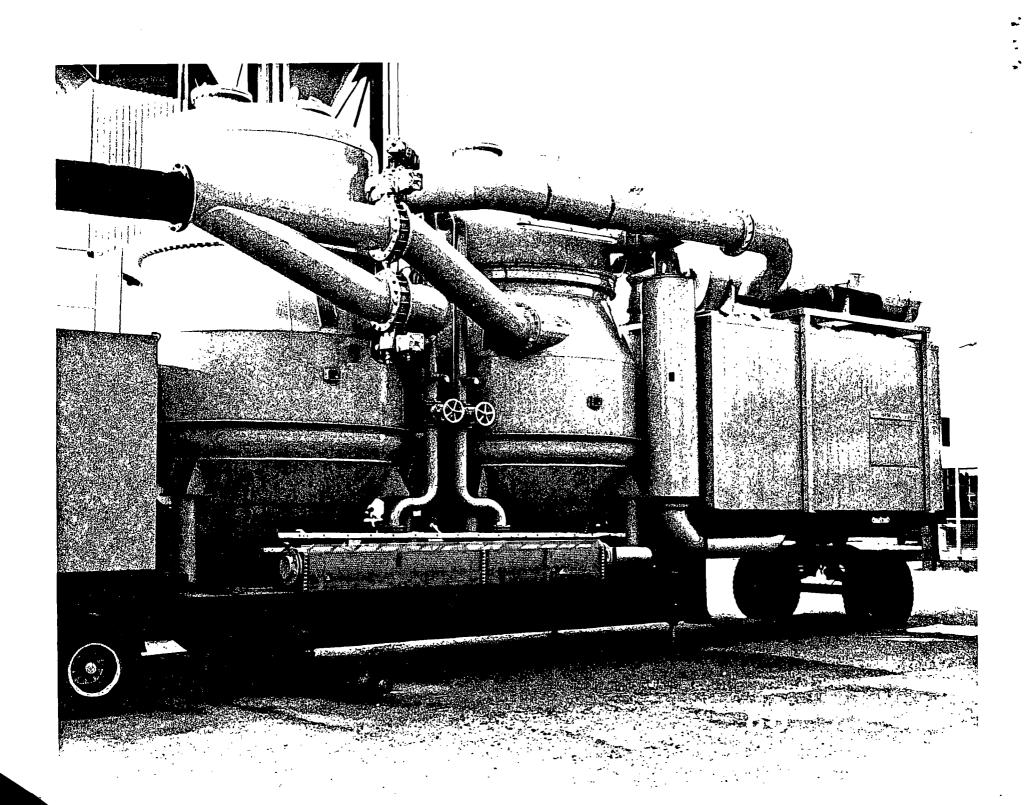
Best Regards,

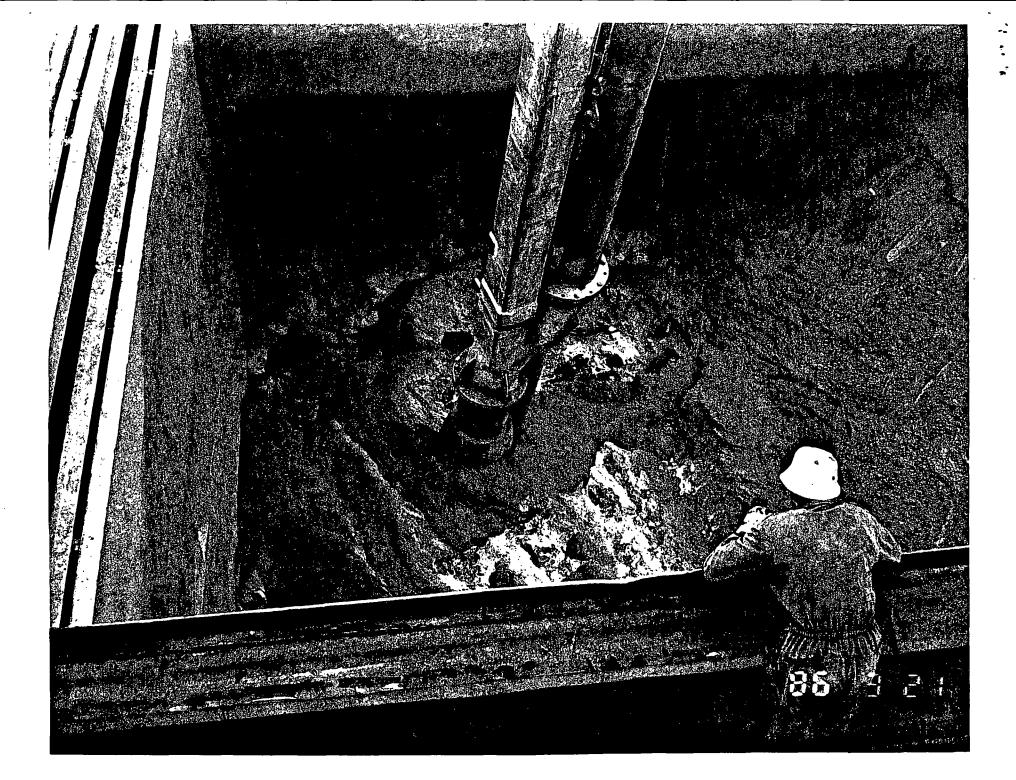
Fred Wuertele

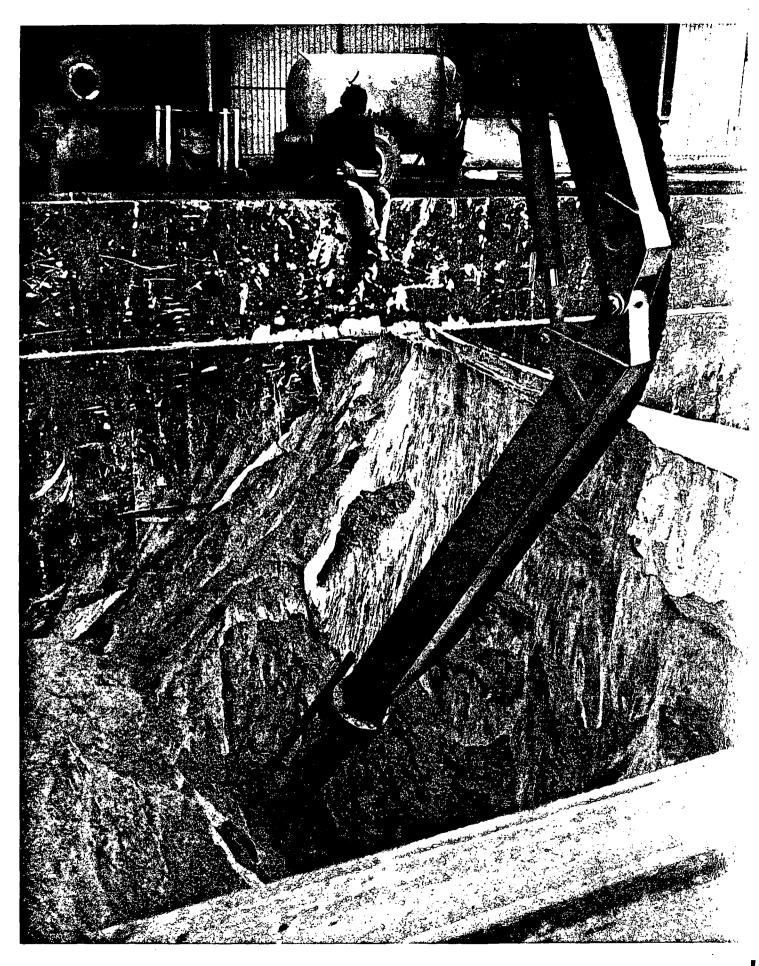
Cyclonaire Corporation

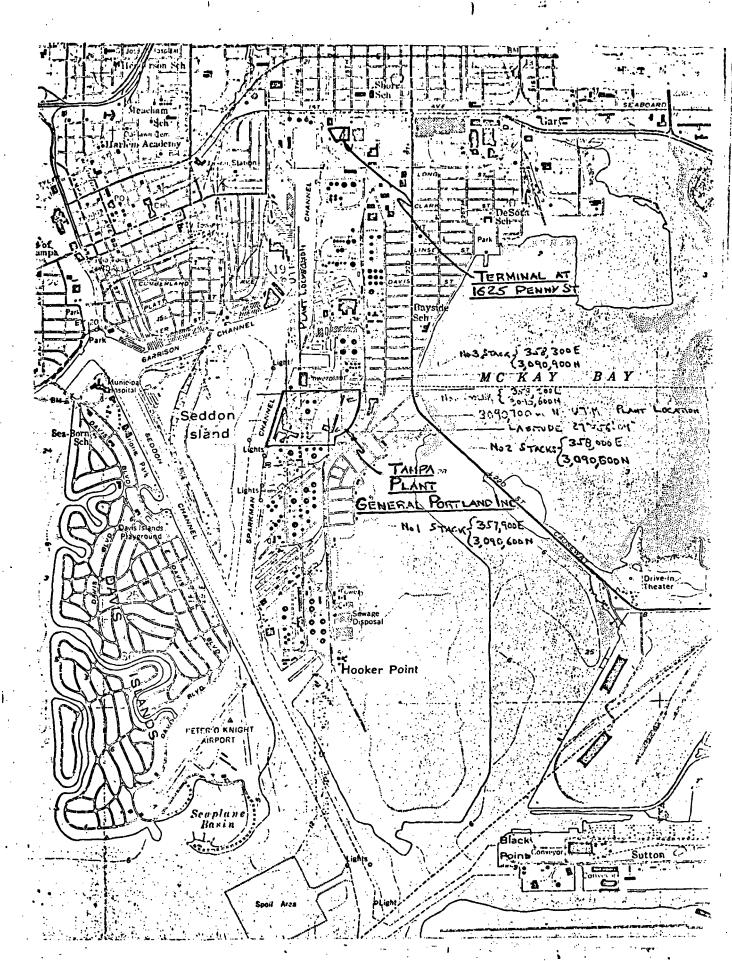
cc: Kovako











### General Portland Inc.

04-085588

State of Florida

PAY: Dept of Environmental Regulation

**VENDOR NO: 29622** 

DATE: 6/277/86

VOUCHER	INVOICE NO.	INVOICE DATE	AMOUNT	DISCOUNT	NET AMOUNT
46483		ee - Modifica C29-094093	tion to Construct	ion	
CHECK NO.					100, 00

General Portland Inc.

04-085588

29622 6/27/86 VENDOR NO.

PAY 0,000,100 DOLLARS 00 CENTS \$ 100.00\*\*\*\*\*\*

NOT VALID AFTER 90 DAYS

San Angelo National Bank

PAY TO THE ORDER OF:

State of Florida Dept. of Environmental Regulation 2200 Blair Stone Rd.

Tallahassee, Fl. 32301

Texas Commerce Bancshares, Inc.



DEPARTMENT OF FLORIDA
DEPARTMENT OF ENVIRONMENTAL REGULATION

RECEIPT FOR APPLICATION FEES AND MISCELLANEOUS REVENUE

Received from Address Date Date
Address Address Dollars \$

Applicant Name & Address Address Application Number Application Number By Application By Application

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