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BUREAU OF AIR REGULATION

**AIR PERMIT APPLICATION AND PREVENTION
OF SIGNIFICANT DETERIORATION ANALYSIS
FOR THE IPS AVON PARK CORPORATION,
HARDEE COUNTY, FLORIDA**

Prepared For:

**IPS Avon Park Corporation
1560 Gulf Blvd., #701
Clearwater, Florida 32767**

Prepared By:

**Golder Associates Inc.
6241 NW 23rd Street, Suite 500
Gainesville, Florida 32653-1500**

**August 1999
9939558Y/F1/WP**

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PART A

AIR PERMIT APPLICATION



Department of Environmental Protection

Division of Air Resources Management

APPLICATION FOR AIR PERMIT - TITLE V SOURCE

See Instructions for Form No. 62-210.900(1)

I. APPLICATION INFORMATION

Identification of Facility

1. Facility Owner/Company Name: IPS Avon Park Corporation	
2. Site Name: IPS Vandolah Power Project	
3. Facility Identification Number: [X] Unknown	
4. Facility Location: Street Address or Other Locator: 2394 Vandolah Road City: Wauchula County: Hardee Zip Code: 33873	
5. Relocatable Facility? [] Yes [X] No	6. Existing Permitted Facility? [] Yes [X] No

Application Contact

1. Name and Title of Application Contact: John S. Ellis	
2. Application Contact Mailing Address: Organization/Firm: IPS Avon Corporation Street Address: 1560 Gulf Blvd., #701 City: Clearwater State: FL Zip Code: 32767	
3. Application Contact Telephone Numbers: Telephone: (727) 517 - 7140 Fax: (727) 517 - 1255	

Application Processing Information (DEP Use)

1. Date of Receipt of Application:	August 31, 1999
2. Permit Number:	0490043-001-AC
3. PSD Number (if applicable):	PSD-FI-275
4. Siting Number (if applicable):	

Purpose of Application

Air Operation Permit Application

This Application for Air Permit is submitted to obtain: (Check one)

- ☐ Initial Title V air operation permit for an existing facility which is classified as a Title V source.
- ☐ Initial Title V air operation permit for a facility which, upon start up of one or more newly constructed or modified emissions units addressed in this application, would become classified as a Title V source.

Current construction permit number: _____

- ☐ Title V air operation permit revision to address one or more newly constructed or modified emissions units addressed in this application.

Current construction permit number: _____

Operation permit number to be revised: _____

- ☐ Title V air operation permit revision or administrative correction to address one or more proposed new or modified emissions units and to be processed concurrently with the air construction permit application. (Also check Air Construction Permit Application below.)

Operation permit number to be revised/corrected: _____

- ☐ Title V air operation permit revision for reasons other than construction or modification of an emissions unit. Give reason for the revision; e.g., to comply with a new applicable requirement or to request approval of an "Early Reductions" proposal.

Operation permit number to be revised: _____

Reason for revision: _____

Air Construction Permit Application

This Application for Air Permit is submitted to obtain: (Check one)

- ☒ Air construction permit to construct or modify one or more emissions units.
- ☐ Air construction permit to make federally enforceable an assumed restriction on the potential emissions of one or more existing, permitted emissions units.
- ☐ Air construction permit for one or more existing, but unpermitted, emissions units.

Owner/Authorized Representative or Responsible Official

1. Name and Title of Owner/Authorized Representative or Responsible Official: John S. Ellis
2. Owner/Authorized Representative or Responsible Official Mailing Address: Organization/Firm: IPS Avon Park Corporation Street Address: 1560 Gulf Blvd., #701 City: Clearwater State: FL Zip Code: 33767
3. Owner/Authorized Representative or Responsible Official Telephone Numbers: Telephone: (727) 517 - 7140 Fax: (727) 517 - 1255
4. Owner/Authorized Representative or Responsible Official Statement: <i>I, the undersigned, am the owner or authorized representative*(check here [], if so) or the responsible official (check here [], if so) of the Title V source addressed in this application, whichever is applicable. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements made in this application are true, accurate and complete and that, to the best of my knowledge, any estimates of emissions reported in this application are based upon reasonable techniques for calculating emissions. The air pollutant emissions units and air pollution control equipment described in this application will be operated and maintained so as to comply with all applicable standards for control of air pollutant emissions found in the statutes of the State of Florida and rules of the Department of Environmental Protection and revisions thereof. I understand that a permit, if granted by the Department, cannot be transferred without authorization from the Department, and I will promptly notify the Department upon sale or legal transfer of any permitted emissions unit.</i> See Attached _____ Signature Date

* Attach letter of authorization if not currently on file.

Professional Engineer Certification

1. Professional Engineer Name: Kennard F. Kosky Registration Number: 14996
2. Professional Engineer Mailing Address: Organization/Firm: Golder Associates Inc. Street Address: 6241 NW 23rd Street, Suite 500 City: Gainesville State: FL Zip Code: 32653-1500
3. Professional Engineer Telephone Numbers: Telephone: (352) 336 - 5600 Fax: (352) 336 - 6603

Owner/Authorized Representative or Responsible Official

1. Name and Title of Owner/Authorized Representative or Responsible Official: John S. Ellis
2. Owner/Authorized Representative or Responsible Official Mailing Address: Organization/Firm: IPS Avon Park Corporation Street Address: 1560 Gulf Blvd., #701 City: Clearwater State: FL Zip Code: 32767
3. Owner/Authorized Representative or Responsible Official Telephone Numbers: Telephone: (727) 517-7140 Fax: (727) 517-1255
4. Owner/Authorized Representative or Responsible Official Statement: <i>I, the undersigned, am the owner or authorized representative* of the non-Title V source addressed in this Application for Air Permit or the responsible official, as defined in Rule 62-210.200, F.A.C., of the Title V source addressed in this application, whichever is applicable. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements made in this application are true, accurate and complete and that, to the best of my knowledge, any estimates of emissions reported in this application are based upon reasonable techniques for calculating emissions. The air pollutant emissions units and air pollution control equipment described in this application will be operated and maintained so as to comply with all applicable standards for control of air pollutant emissions found in the statutes of the State of Florida and rules of the Department of Environmental Protection and revisions thereof. I understand that a permit, if granted by the Department, cannot be transferred without authorization from the Department, and I will promptly notify the Department upon sale or legal transfer of any permitted emissions unit.</i> <div style="display: flex; justify-content: space-between;"><div>Signature <u>John S. Ellis</u></div><div>Date <u>8-25-99</u></div></div>

* Attach letter of authorization if not currently on file.

4. Professional Engineer Statement:

I, the undersigned, hereby certify, except as particularly noted herein, that:*

(1) To the best of my knowledge, there is reasonable assurance that the air pollutant emissions unit(s) and the air pollution control equipment described in this Application for Air Permit, when properly operated and maintained, will comply with all applicable standards for control of air pollutant emissions found in the Florida Statutes and rules of the Department of Environmental Protection; and

(2) To the best of my knowledge, any emission estimates reported or relied on in this application are true, accurate, and complete and are either based upon reasonable techniques available for calculating emissions or, for emission estimates of hazardous air pollutants not regulated for an emissions unit addressed in this application, based solely upon the materials, information and calculations submitted with this application.

If the purpose of this application is to obtain a Title V source air operation permit (check here [☐], if so), I further certify that each emissions unit described in this Application for Air Permit, when properly operated and maintained, will comply with the applicable requirements identified in this application to which the unit is subject, except those emissions units for which a compliance schedule is submitted with this application.

If the purpose of this application is to obtain an air construction permit for one or more proposed new or modified emissions units (check here [☒], if so), I further certify that the engineering features of each such emissions unit described in this application have been designed or examined by me or individuals under my direct supervision and found to be in conformity with sound engineering principles applicable to the control of emissions of the air pollutants characterized in this application.

If the purpose of this application is to obtain an initial air operation permit or operation permit revision for one or more newly constructed or modified emissions units (check here [☐], if so), I further certify that, with the exception of any changes detailed as part of this application, each such emissions unit has been constructed or modified in substantial accordance with the information given in the corresponding application for air construction permit and with all provisions contained in such permit.

Signature

Date

(seal)

Attach any exception to certification statement.

Scope of Application

Emissions Unit ID	Description of Emissions Unit	Permit Type	Processing Fee
1R	GE Frame 7FA Combustion Turbine	AC1A	
2R	GE Frame 7FA Combustion Turbine	AC1A	
3R	GE Frame 7FA Combustion Turbine	AC1A	
4R	GE Frame 7FA Combustion Turbine	AC1A	
5	Unregulated Emissions	AC1A	

Application Processing Fee

Check one: ☒ Attached - Amount: \$: 7,500 ☐ Not Applicable

Construction/Modification Information

1. Description of Proposed Project or Alterations:

Construction of 4 170-MW 'F' Class combustion turbines. See Attachment PSD-IPS.

2. Projected or Actual Date of Commencement of Construction: **1 Jul 2000**

3. Projected Date of Completion of Construction: **1 Jan 2002**

Application Comment

See Attachment PSD-IPS

II. FACILITY INFORMATION

A. GENERAL FACILITY INFORMATION

Facility Location and Type

1. Facility UTM Coordinates: Zone: 17 East (km): 408.75 North (km): 3044.5			
2. Facility Latitude/Longitude: Latitude (DD/MM/SS): 27 / 31 / 22 Longitude (DD/MM/SS): 81 / 55 / 28			
3. Governmental Facility Code: 0	4. Facility Status Code: C	5. Facility Major Group SIC Code: 49	6. Facility SIC(s): 4911
7. Facility Comment (limit to 500 characters): Project consists of four 170-MW dual-fuel, General Electric Frame 7FA combustion turbines that will use dry low-nitrogen oxide combustion technology when firing natural gas and water injection when firing distillate fuel oil. Each CT will operate up to 3,390 hours per year.			

Facility Contact

1. Name and Title of Facility Contact: Mr. John S. Ellis, President			
2. Facility Contact Mailing Address: Organization/Firm: IPS Avon Park Corporation Street Address: 1560 Gulf Blvd., #701 City: Clearwater State: FL Zip Code: 33767			
3. Facility Contact Telephone Numbers: Telephone: (727) 517 - 7140 Fax: (727) 517 - 1255			

Facility Regulatory Classifications**Check all that apply:**

1. <input type="checkbox"/> Small Business Stationary Source?	<input type="checkbox"/> Unknown
2. <input checked="" type="checkbox"/> Major Source of Pollutants Other than Hazardous Air Pollutants (HAPs)?	
3. <input type="checkbox"/> Synthetic Minor Source of Pollutants Other than HAPs?	
4. <input type="checkbox"/> Major Source of Hazardous Air Pollutants (HAPs)?	
5. <input type="checkbox"/> Synthetic Minor Source of HAPs?	
6. <input checked="" type="checkbox"/> One or More Emissions Units Subject to NSPS?	
7. <input type="checkbox"/> One or More Emission Units Subject to NESHAP?	
8. <input checked="" type="checkbox"/> Title V Source by EPA Designation?	
9. Facility Regulatory Classifications Comment (limit to 200 characters): CT is subject to NSPS Subpart GG. The tanks are subject to Subpart Kb.	

List of Applicable Regulations

Not Applicable	

Figure 1 illustrates the experimental setup. A subject is seated at a table, viewing a video screen. A camera is positioned above the screen. A target is placed on the table. A horizontal arrow indicates the movement of the hand from the starting position to the target. A vertical arrow indicates the movement of the hand from the starting position to the video screen. A horizontal arrow indicates the movement of the hand from the video screen to the target. A vertical arrow indicates the movement of the hand from the video screen to the camera.

List of Pollutants Emitted

[illegible]

Age group	Percentage of correct responses
4-5	85
6-7	90
8-9	95
10-11	98
12-13	100

Supplemental Requirements

1. Area Map Showing Facility Location: [X] Attached, Document ID: <u>PSD-IPS</u> [] Not Applicable [] Waiver Requested
2. Facility Plot Plan: [X] Attached, Document ID: <u>PSD-IPS</u> [] Not Applicable [] Waiver Requested
3. Process Flow Diagram(s): [X] Attached, Document ID: <u>PSD-IPS</u> [] Not Applicable [] Waiver Requested
4. Precautions to Prevent Emissions of Unconfined Particulate Matter: [] Attached, Document ID: _____ [X] Not Applicable [] Waiver Requested
5. Fugitive Emissions Identification: [] Attached, Document ID: _____ [X] Not Applicable [] Waiver Requested
6. Supplemental Information for Construction Permit Application: [X] Attached, Document ID: <u>PSD-IPS</u> [] Not Applicable
7. Supplemental Requirements Comment:

Additional Supplemental Requirements for Title V Air Operation Permit Applications

8. List of Proposed Insignificant Activities: <input type="checkbox"/> Attached, Document ID:_____ <input type="checkbox"/> Not Applicable
9. List of Equipment/Activities Regulated under Title VI: <input type="checkbox"/> Attached, Document ID:_____ <input type="checkbox"/> Equipment/Activities On site but Not Required to be Individually Listed <input type="checkbox"/> Not Applicable
10. Alternative Methods of Operation: <input type="checkbox"/> Attached, Document ID:_____ <input type="checkbox"/> Not Applicable
11. Alternative Modes of Operation (Emissions Trading): <input type="checkbox"/> Attached, Document ID:_____ <input type="checkbox"/> Not Applicable
12. Identification of Additional Applicable Requirements: <input type="checkbox"/> Attached, Document ID:_____ <input type="checkbox"/> Not Applicable
13. Risk Management Plan Verification: <input type="checkbox"/> Plan previously submitted to Chemical Emergency Preparedness and Prevention Office (CEPPO). Verification of submittal attached (Document ID:_____) or previously submitted to DEP (Date and DEP Office:_____) <input type="checkbox"/> Plan to be submitted to CEPPO (Date required:_____) <input type="checkbox"/> Not Applicable
14. Compliance Report and Plan: <input type="checkbox"/> Attached, Document ID:_____ <input type="checkbox"/> Not Applicable
15. Compliance Certification (Hard-copy Required): <input type="checkbox"/> Attached, Document ID:_____ <input type="checkbox"/> Not Applicable

III. EMISSIONS UNIT INFORMATION

A separate Emissions Unit Information Section (including subsections A through J as required) must be completed for each emissions unit addressed in this Application for Air Permit. If submitting the application form in hard copy, indicate, in the space provided at the top of each page, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application.

A. GENERAL EMISSIONS UNIT INFORMATION
(All Emissions Units)

Emissions Unit Description and Status

1. Type of Emissions Unit Addressed in This Section: (Check one)			
<input checked="" type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).			
<input type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.			
<input type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only.			
2. Regulated or Unregulated Emissions Unit? (Check one)			
<input checked="" type="checkbox"/> The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.			
<input type="checkbox"/> The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.			
3. Description of Emissions Unit Addressed in This Section (limit to 60 characters):			
GE Frame 7FA Combustion Turbine			
4. Emissions Unit Identification Number:		<input type="checkbox"/> No ID <input checked="" type="checkbox"/> ID Unknown	
5. Emissions Unit Status Code:	6. Initial Startup Date:	7. Emissions Unit Major Group SIC Code:	8. Acid Rain Unit?
C		49	<input checked="" type="checkbox"/>
9. Emissions Unit Comment: (Limit to 500 Characters)			
This emission unit is a GE Frame 7FA combustion turbine operating in simple cycle mode. See Attachment PSD-IPS.			

Emissions Unit Control Equipment

1. Control Equipment/Method Description (Limit to 200 characters per device or method):

Dry Low NO_x combustion - Natural gas firing2. Control Device or Method Code(s): **25****Emissions Unit Details**

1. Package Unit:

Manufacturer: **General Electric**Model Number: **7FA**

2. Generator Nameplate Rating:

172 MW

3. Incinerator Information:

Dwell Temperature:

°F

Dwell Time:

seconds

Incinerator Afterburner Temperature:

°F

Emissions Unit Control Equipment

1. Control Equipment/Method Description (Limit to 200 characters per device or method):

Water Injection - distillate oil firing2. Control Device or Method Code(s): **28****Emissions Unit Details**

1. Package Unit:

Manufacturer: **General Electric**Model Number: **7FA**

2. Generator Nameplate Rating:

172 MW

3. Incinerator Information:

Dwell Temperature:

°F

Dwell Time:

seconds

Incinerator Afterburner Temperature:

°F

B. EMISSIONS UNIT CAPACITY INFORMATION
(Regulated Emissions Units Only)**Emissions Unit Operating Capacity and Schedule**

1. Maximum Heat Input Rate:	1,612	mmBtu/hr
2. Maximum Incineration Rate:	lb/hr	tons/day
3. Maximum Process or Throughput Rate:		
4. Maximum Production Rate:		
5. Requested Maximum Operating Schedule:		
	hours/day	days/week
	weeks/year	3,390 hours/year
6. Operating Capacity/Schedule Comment (limit to 200 characters):		
Maximum heat input at ISO conditions and natural gas firing (LHV); maximum for oil firing is 1,806 MMBtu/hr (ISO-LHV) and 182 MW.		

C. EMISSIONS UNIT REGULATIONS
(Regulated Emissions Units Only)**List of Applicable Regulations**

See Attachment IPS-EU1-D for operational requirements	
See Attachment PSD-IPS for permitting requirements	

ATTACHMENT IPS-EU1-D

Applicable Requirements Listing

EMISSION UNIT ID: EU1

FDEP Rules:

Air Pollution Control-General Provisions:

- 62-204.800(7)(b)37. (State Only) - NSPS Subpart GG
- 62-204.800(7)(c) (State Only) - NSPS authority
- 62-204.800(7)(d)(State Only) - NSPS General Provisions
- 62-204.800(12) (State Only) - Acid Rain Program
- 62-204.800(13) (State Only) - Allowances
- 62-204.800(14) (State Only) - Acid Rain Program Monitoring
- 62-204.800(16) (State Only) - Excess Emissions (Potentially applicable over term of permit)

Stationary Sources-General:

- 62-210.650 - Circumvention; EUs with control device
- 62-210.700(1) - Excess Emissions;
- 62-210.700(4) - Excess Emissions; poor maintenance
- 62-210.700(6) - Excess Emissions; notification

Acid Rain:

- 62-214.300 - All Acid Rain Units (Applicability)
- 62-214.320(1)(a),(2) - All Acid Rain Units (Application Shield)
- 62-214.330(1)(a)1. - Compliance Options (if 214.430)
- 62-214.340 - Exemptions (new units, retired units)
- 62-214.350(2);(3);(6) - All Acid Rain Units (Certification)
- 62-214.370 - All Acid Rain Units (Revisions; correction; potentially applicable if a need arises)
- 62-214.430 - All Acid Rain Units (Compliance Options-if required)

Stationary Sources-Emission Standards:

- 62-296.320(4)(b)(State Only) - CTs/Diesel Units

Stationary Sources-Emission Monitoring (where stack test is required):

- 62-297.310(1) - All Units (Test Runs-Mass Emission)
- 62-297.310(2)(b) - All Units (Operating Rate; other than CTs;no CT)
- 62-297.310(3) - All Units (Calculation of Emission)
- 62-297.310(4)(a) - All Units (Applicable Test Procedures;Sampling time)
- 62-297.310(4)(b) - All Units (Sample Volume)
- 62-297.310(4)(c) - All Units (Required Flow Rate Range-PM/H2SO4/F)
- 62-297.310(4)(d) - All Units (Calibration)
- 62-297.310(4)(e) - All Units (EPA Method 5-only)

- 62-297.310(5)
 - 62-297.310(6)(a)
 - 62-297.310(6)(c)
 - 62-297.310(6)(d)
 - 62-297.310(6)(e)
 - 62-297.310(6)(f)
 - 62-297.310(6)(g)
 - 62-297.310(7)(a)1.
 - 62-297.310(7)(a)2.
 - 62-297.310(7)(a)3.
 - 62-297.310(7)(a)4.a
 - 62-297.310(7)(a)5.
 - 62-297.310(7)(a)6.
 - 62-297.310(7)(a)7.
 - 62-297.310(7)(a)9.
 - 62-297.310(7)(c)
 - 62-297.310(8)
- All Units (Determination of Process Variables)
 - All Units (Permanent Test Facilities-general)
 - All Units (Sampling Ports)
 - All Units (Work Platforms)
 - All Units (Access)
 - All Units (Electrical Power)
 - All Units (Equipment Support)
 - Applies mainly to CTs/Diesels
 - FFSG excess emissions
 - Permit Renewal Test Required
 - Annual Test
 - PM exemption if <400 hrs/yr
 - PM FFSG semi annual test required if >200 hrs/yr
 - PM quarterly monitoring if >100 hrs/yr
 - FDEP Notification - 15 days
 - Waiver of Compliance Tests (Fuel Sampling)
 - Test Reports

Federal Rules:

NSPS Subpart GG:

- 40 CFR 60.332(a)(1)
 - 40 CFR 60.332(a)(3)
 - 40 CFR 60.333
 - 40 CFR 60.334
 - 40 CFR 60.335
- NOx for Electric Utility CTs
 - NOx for Electric Utility CTs
 - SO2 limits
 - Monitoring of Operations (Custom Monitoring for Gas)
 - Test Methods

NSPS General Requirements:

- 40 CFR 60.7(a)(1)
 - 40 CFR 60.7(a)(2)
 - 40 CFR 60.7(a)(3)
 - 40 CFR 60.7(a)(4)
 - Cycle)
 - 40 CFR 60.7(a)(5)
 - 40 CFR 60.7(b)
 - (startup/shutdown/malfunction)
 - 40 CFR 60.7(c)
 - (startup/shutdown/malfunction)
 - 40 CFR 60.7(d)
 - (startup/shutdown/malfunction)
 - 40 CFR 60.7(f)
 - 40 CFR 60.8(a)
 - 40 CFR 60.8(b)
 - 40 CFR 60.8(c)
 - 40 CFR 60.8(e)
 - 40 CFR 60.8(f)
- Notification of Construction
 - Notification of Initial Start-Up
 - Notification of Actual Start-Up
 - Notification and Recordkeeping (Physical/Operational
 - Notification of CEM Demonstration
 - Notification and Recordkeeping
 - Notification and Recordkeeping
 - Notification and Recordkeeping (maintain records-2 yrs)
 - Performance Test Requirements
 - Performance Test Notification
 - Performance Tests (representative conditions)
 - Provide Stack Sampling Facilities
 - Test Runs

40 CFR 60.11(a)	- Compliance (ref. S. 60.8 or Subpart; other than opacity)
40 CFR 60.11(b)	- Compliance (opacity determined EPA Method 9)
40 CFR 60.11(c)	- Compliance (opacity; excludes
startup/shutdown/malfunction)	
40 CFR 60.11(d)	- Compliance (maintain air pollution control equip.)
40 CFR 60.11(e)(2)	- Compliance (opacity; ref. S. 60.8)
40 CFR 60.12	- Circumvention
40 CFR 60.13(a)	- Monitoring (Appendix B; Appendix F)
40 CFR 60.13(c)	- Monitoring (Opacity COMS)
40 CFR 60.13(d)(1)	- Monitoring (CEMS; span, drift, etc.)
40 CFR 60.13(d)(2)	- Monitoring (COMS; span, system check)
40 CFR 60.13(e)	- Monitoring (frequency of operation)
40 CFR 60.13(f)	- Monitoring (frequency of operation)
40 CFR 60.13(h)	- Monitoring (COMS; data requirements)
Acid Rain-Permits:	
40 CFR 72.9(a)	- Permit Requirements
40 CFR 72.9(b)	- Monitoring Requirements
40 CFR 72.9(c)(1)	- SO2 Allowances-hold allowances
40 CFR 72.9(c)(2)	- SO2 Allowances-violation
40 CFR 72.9(c)(3)(iii)	- SO2 Allowances-Phase II Units (listed)
40 CFR 72.9(c)(4)	- SO2 Allowances-allowances held in ATS
40 CFR 72.9(c)(5)	- SO2 Allowances-no deduction for 72.9(c)(1)(i)
40 CFR 72.9(d)	- NOx Requirements
40 CFR 72.9(e)	- Excess Emission Requirements
40 CFR 72.9(f)	- Recordkeeping and Reporting
40 CFR 72.9(g)	- Liability
40 CFR 72.20(a)	- Designated Representative; required
40 CFR 72.20(b)	- Designated Representative; legally binding
40 CFR 72.20(c)	- Designated Representative; certification requirements
40 CFR 72.21	- Submissions
40 CFR 72.22	- Alternate Designated Representative
40 CFR 72.23	- Changing representatives; owners
40 CFR 72.24	- Certificate of representation
40 CFR 72.30(a)	- Requirements to Apply (operate)
40 CFR 72.30(b)(2)	- Requirements to Apply (Phase II-Complete)
40 CFR 72.30(c)	- Requirements to Apply (reapply before expiration)
40 CFR 72.30(d)	- Requirements to Apply (submittal requirements)
40 CFR 72.31	- Information Requirements; Acid Rain Applications
40 CFR 72.32	- Permit Application Shield
40 CFR 72.33(b)	- Dispatch System ID;unit/system ID
40 CFR 72.33(c)	- Dispatch System ID;ID requirements
40 CFR 72.33(d)	- Dispatch System ID;ID change
40 CFR 72.40(a)	- General; compliance plan
40 CFR 72.40(b)	- General; multi-unit compliance options
40 CFR 72.40(c)	- General; conditional approval

40 CFR 72.40(d)
40 CFR 72.51
40 CFR 72.90

- General; termination of compliance options
- Permit Shield
- Annual Compliance Certification

Allowances:

40 CFR 73.33(a),(c)
40 CFR 73.35(c)(1)

- Authorized account representative
- Compliance: ID of allowances by serial number

Monitoring Part 75:

40 CFR 75.4
40 CFR 75.5
40 CFR 75.10(a)(1)
40 CFR 75.10(a)(2)
40 CFR 75.10(a)(3)(iii)
40 CFR 75.10(b)
40 CFR 75.10(c)
40 CFR 75.10(e)
40 CFR 75.10(f)
40 CFR 75.10(g)
40 CFR 75.11(d)
40 CFR 75.11(e)
40 CFR 75.12(a)
40 CFR 75.12(b)

- Compliance Dates;
- Prohibitions
- Primary Measurement; SO₂;
- Primary Measurement; NO_x;
- Primary Measurement; CO₂; O₂ monitor
- Primary Measurement; Performance Requirements
- Primary Measurement; Heat Input; Appendix F
- Primary Measurement; Optional Backup Monitor
- Primary Measurement; Minimum Measurement
- Primary Measurement; Minimum Recording
- SO₂ Monitoring; Gas- and Oil-fired units
- SO₂ Monitoring; Gaseous firing
- NO_x Monitoring; Coal; Non-peaking oil/gas units
- NO_x Monitoring; Determination of NO_x emission rate; Appendix F

40 CFR 75.13(b)
40 CFR 75.13(c)
40 CFR 75.14(c)
40 CFR 75.20(a)
Certification

- CO₂ Monitoring; Appendix G
- CO₂ Monitoring; Appendix F
- Opacity Monitoring; Gas units; exemption
- Initial Certification Approval Process; Loss of

40 CFR 75.20(b)
40 CFR 75.20(c)
40 CFR 75.20(d)
40 CFR 75.20(f)
40 CFR 75.21(a)
12/31/96)

- Recertification Procedures (if recertification necessary)
- Certification Procedures (if recertification necessary)
- Recertification Backup/portable monitor
- Alternate Monitoring system
- QA/QC; CEMS; Appendix B (Suspended 7/17/95-

40 CFR 75.21(c)
40 CFR 75.21(d)
40 CFR 75.21(e)
40 CFR 75.21(f)
40 CFR 75.22
40 CFR 75.24

- QA/QC; Calibration Gases
- QA/QC; Notification of RATA
- QA/QC; Audits
- QA/QC; CEMS (Effective 7/17/96-12/31/96)
- Reference Methods

40 CFR 75.30(a)(3)
40 CFR 75.30(a)(4)
40 CFR 75.30(b)
monitor

- Out-of-Control Periods; CEMS
- General Missing Data Procedures; NO_x
- General Missing Data Procedures; SO₂
- General Missing Data Procedures; certified backup

40 CFR 75.30(c)
monitor

- General Missing Data Procedures; certified backup

- 40 CFR 75.30(d)
 - 40 CFR 75.30(e)
stacks
 - 40 CFR 75.31
 - 40 CFR 75.32
 - 40 CFR 75.33
 - 40 CFR 75.36
 - 40 CFR 75.40
 - 40 CFR 75.41
 - 40 CFR 75.42
 - 40 CFR 75.43
 - 40 CFR 75.44
 - 40 CFR 75.45
 - 40 CFR 75.46
 - 40 CFR 75.47
 - 40 CFR 75.48
 - 40 CFR 75.53
 - 40 CFR 75.54(a)
 - 40 CFR 75.54(b)
 - 40 CFR 75.54(c)
 - 40 CFR 75.54(d)
 - 40 CFR 75.54(e)
 - 40 CFR 75.54(f)
 - 40 CFR 75.55(c)
 - 40 CFR 75.55(e)
 - 40 CFR 75.56
 - 40 CFR 75.60
 - 40 CFR 75.61
 - 40 CFR 75.62
 - 40 CFR 75.63
 - 40 CFR 75.64(a)
 - 40 CFR 75.64(b)
statement
 - 40 CFR 75.64(c)
 - 40 CFR 75.64(d)
 - 40 CFR 75.66
 - Appendix A-1
 - Appendix A-2.
 - Appendix A-3.
 - Appendix A-4.
 - Appendix A-5.
 - Appendix A-6.
 - Appendix A-7.
 - Appendix B
 - Appendix C-1.
 - Appendix C-2.
- General Missing Data Procedures; SO₂ (optional before 1/1/97)
 - General Missing Data Procedures; bypass/multiple
 - Initial Missing Data Procedures (new/re-certified CMS)
 - Monitoring Data Availability for Missing Data
 - Standard Missing Data Procedures
 - Missing Data for Heat Input
 - Alternate Monitoring Systems-General
 - Alternate Monitoring Systems-Precision Criteria
 - Alternate Monitoring Systems-Reliability Criteria
 - Alternate Monitoring Systems-Accessability Criteria
 - Alternate Monitoring Systems-Timeliness Criteria
 - Alternate Monitoring Systems-Daily QA
 - Alternate Monitoring Systems-Missing data
 - Alternate Monitoring Systems-Criteria for Class
 - Alternate Monitoring Systems-Petition
 - Monitoring Plan ; revisions
 - Recordkeeping-general
 - Recordkeeping-operating parameter
 - Recordkeeping-SO₂
 - Recordkeeping-NO_x
 - Recordkeeping-CO₂
 - Recordkeeping-Opacity
 - General Recordkeeping (Specific Situations)
 - General Recordkeeping (Specific Situations)
 - Certification; QA/QC Provisions
 - Reporting Requirements-General
 - Reporting Requirements-Notification cert/recertification
 - Reporting Requirements-Monitoring Plan
 - Reporting Requirements-Certification/Recertification
 - Reporting Requirements-Quarterly reports; submission
 - Reporting Requirements-Quarterly reports; DR
 - Rep. Req.; Quarterly reports; Compliance Certification
 - Rep. Req.; Quarterly reports; Electronic format
 - Petitions to the Administrator (if required)
 - Installation and Measurement Locations
 - Equipment Specifications
 - Performance Specifications
 - Data Handling and Acquisition Systems
 - Calibration Gases
 - Certification Tests and Procedures
 - Calculations
 - QA/QC Procedures
 - Missing Data; SO₂/NO_x for controlled sources
 - Missing Data; Load-Based Procedure; NO_x & flow

Appendix D
Appendix F
Appendix H

- Optional SO₂; Oil-/gas-fired units
- Conversion Procedures
- Traceability Protocol

Acid Rain Program-Excess Emissions (these are future requirements):

40 CFR 77.3

- Offset Plans (future)

40 CFR 77.5(b)

- Deductions of Allowances (future)

40 CFR 77.6

- Excess Emissions Penalties (SO₂ and NO_x;future)

D. EMISSION POINT (STACK/VENT) INFORMATION
(Regulated Emissions Units Only)**Emission Point Description and Type**

1. Identification of Point on Plot Plan or Flow Diagram? See Att. PSD-IPS		2. Emission Point Type Code: 1	
3. Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking (limit to 100 characters per point): Exhausts through a single stack.			
4. ID Numbers or Descriptions of Emission Units with this Emission Point in Common:			
5. Discharge Type Code: V	6. Stack Height: 60 feet	7. Exit Diameter: 22 feet	
8. Exit Temperature: 1,113 °F	9. Actual Volumetric Flow Rate: 2,645,000 acfm	10. Water Vapor: 8.6 %	
11. Maximum Dry Standard Flow Rate: 300,000 dscfm		12. Nonstack Emission Point Height: feet	
13. Emission Point UTM Coordinates: Zone: 17 East (km): 408.75 North (km): 3044.50			
14. Emission Point Comment (limit to 200 characters): Stack parameters for ISO operating condition firing natural gas; for oil 1,094°F and 2,731,000 ACFM.			

E. SEGMENT (PROCESS/FUEL) INFORMATION
(All Emissions Units)**Segment Description and Rate:** Segment 1 of 2

1. Segment Description (Process/Fuel Type) (limit to 500 characters): Distillate (No. 2) Fuel Oil		
2. Source Classification Code (SCC): 20100101		3. SCC Units: 1,000 gallons used
4. Maximum Hourly Rate: 13.9	5. Maximum Annual Rate: 13,900	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur: 0.05	8. Maximum % Ash:	9. Million Btu per SCC Unit: 132
10. Segment Comment (limit to 200 characters): Million Btu per SCC Unit = 131.8 (rounded to 132). Based on 7.1 lb/gal; LHV of 18,560 Btu/lb, - ISO conditions, 1,000 hrs/yr operation.		

Segment Description and Rate: Segment 2 of 2

1. Segment Description (Process/Fuel Type) (limit to 500 characters): Natural Gas		
2. Source Classification Code (SCC): 20100201		3. SCC Units: Million Cubic Feet
4. Maximum Hourly Rate: 1.70	5. Maximum Annual Rate: 5,752	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur:	8. Maximum % Ash:	9. Million Btu per SCC Unit: 950
10. Segment Comment (limit to 200 characters): Based on 950 Btu/cf (LHV); ISO conditions and 3,390 hrs/yr operation.		

F. EMISSIONS UNIT POLLUTANTS
(All Emissions Units)

1. Pollutant Emitted	2. Primary Control Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
PM			EL
SO ₂			EL
NO _x	026	028	EL
CO			EL
VOC			EL
PM ₁₀			EL

G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION

(Regulated Emissions Units -
Emissions-Limited and Preconstruction Review Pollutants Only)

Potential/Fugitive Emissions

1. Pollutant Emitted: PM	2. Total Percent Efficiency of Control:
3. Potential Emissions: 17 lb/hour 20.5 tons/year	4. Synthetically Limited? [X]
5. Range of Estimated Fugitive Emissions: [] 1 [] 2 [] 3 _____ to _____ tons/year	
6. Emission Factor: Reference: GE, 1998; Golder	7. Emissions Method Code: 2
8. Calculation of Emissions (limit to 600 characters): See Attachment PSD-IPS; Section 2.0; Appendix A.	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters): Lb/hr based on oil firing, all loads. Tons/year based on 2,390 hrs/yr gas firing and 1,000 hrs/yr oil firing; ISO conditions.	

Allowable Emissions Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: 17 lb/hr	4. Equivalent Allowable Emissions: 17 lb/hour 8.5 tons/year
5. Method of Compliance (limit to 60 characters): Annual stack test; EPA Methods 5 or 17; if < 400 hours	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters): Oil firing - all loads; 1,000 hrs/yr. See Attachment PSD-IPS; Section 2.0; Appendix A.	

G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION
(Regulated Emissions Units -
Emissions-Limited and Preconstruction Review Pollutants Only)

Potential/Fugitive Emissions

1. Pollutant Emitted: PM	2. Total Percent Efficiency of Control:	
3. Potential Emissions: 17 lb/hour 20.5 tons/year	4. Synthetically Limited? [X]	
5. Range of Estimated Fugitive Emissions: [] 1 [] 2 [] 3 _____ to _____ tons/year		
6. Emission Factor: Reference: GE, 1998; Golder		7. Emissions Method Code: 2
8. Calculation of Emissions (limit to 600 characters): See Attachment PSD-IPS; Section 2.0; Appendix A.		
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters): Lb/hr based on oil firing, all loads. Tons/year based on 2,390 hrs/yr gas firing and 1,000 hrs/yr oil firing; ISO conditions.		

Allowable Emissions Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: 10 lb/hr	4. Equivalent Allowable Emissions: 10 lb/hour 17 tons/year
5. Method of Compliance (limit to 60 characters): VE Test < 20% opacity	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters): Gas firing - all loads; 3,390 hrs/yr. See Attachment PSD-IPS; Section 2.0; Appendix A.	

G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION
(Regulated Emissions Units -
Emissions-Limited and Preconstruction Review Pollutants Only)

Potential/Fugitive Emissions

1. Pollutant Emitted: SO₂	2. Total Percent Efficiency of Control:
3. Potential Emissions: 101.5 lb/hour 55.3 tons/year	4. Synthetically Limited? [X]
5. Range of Estimated Fugitive Emissions: [] 1 [] 2 [] 3 _____ to _____ tons/year	
6. Emission Factor: Reference: GE, 1998; Golder	7. Emissions Method Code: 2
8. Calculation of Emissions (limit to 600 characters): See Attachment PSD-IPS; Section 2.0; Appendix A.	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters): Emission Factor: 1 grain S per 100 CF gas; 0.05% S oil lb/hr based on oil firing, 100% load, 32°F. Tons/yr based on 2,390 hrs/yr gas firing and 1,000 hrs/yr oil firing, ISO conditions.	

Allowable Emissions Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: 0.05 % Sulfur Oil	4. Equivalent Allowable Emissions: 101.5 lb/hour 49.3 tons/year
5. Method of Compliance (limit to 60 characters): Fuel Sampling	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters): Oil firing - 32°F; 100% load; 1,000 hrs/yr. See Attachment PSD-IPS; Section 2.0; Appendix A.	

G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION
(Regulated Emissions Units -
Emissions-Limited and Preconstruction Review Pollutants Only)

Potential/Fugitive Emissions

1. Pollutant Emitted: SO₂	2. Total Percent Efficiency of Control:	
3. Potential Emissions: 101.5 lb/hour 55.3 tons/year	4. Synthetically Limited? [X]	
5. Range of Estimated Fugitive Emissions: [] 1 [] 2 [] 3 _____ to _____ tons/year		
6. Emission Factor: Reference: GE, 1998; Golder	7. Emissions Method Code: 2	
8. Calculation of Emissions (limit to 600 characters): See Attachment PSD-IPS; Section 2.0; Appendix A.		
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters): Emission Factor: 1 grain S per 100 CF gas; 0.05% S oil lb/hr based on oil firing, 100% load, 32°F. Tons/yr based on 2,390 hrs/yr gas firing and 1,000 hrs/yr oil firing, ISO conditions.		

Allowable Emissions Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: See Comment	4. Equivalent Allowable Emissions: 5.1 lb/hour 8.4 tons/year
5. Method of Compliance (limit to 60 characters): Fuel Sampling	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters): Requested allowable emissions and units: Pipeline Natural Gas. Gas firing, 1 gram/100 cf - 32°F, 100% load; 3,390 hrs/yr. See Attachment PSD-IPS; Section 2.0; Appendix A.	

G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION

(Regulated Emissions Units -

Emissions-Limited and Preconstruction Review Pollutants Only)

Potential/Fugitive Emissions

1. Pollutant Emitted: NO_x	2. Total Percent Efficiency of Control:
3. Potential Emissions: 362 lb/hour 252 tons/year	4. Synthetically Limited? [X]
5. Range of Estimated Fugitive Emissions: [] 1 [] 2 [] 3 _____ to _____ tons/year	
6. Emission Factor: Reference: GE, 1998; Golder	7. Emissions Method Code: 2
8. Calculation of Emissions (limit to 600 characters): See Attachment PSD-IPS; Section 2.0; Appendix A.	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters): Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,390 hrs/yr gas firing and 1,000 hrs/yr oil firing; ISO conditions.	

Allowable Emissions Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: 42 ppmvd	4. Equivalent Allowable Emissions: 362.0 lb/hour 175.4 tons/year
5. Method of Compliance (limit to 60 characters): CEM - 30 Day Rolling Average	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters): Requested Allowable Emissions is at 15% O2-100% load. Oil firing; max @ 32°F; 100% load; TPY @ 59°F, 1,000 hrs/yr. See Attachment PSD-IPS; Section 2.0; Appendix A.	

G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION
(Regulated Emissions Units -
Emissions-Limited and Preconstruction Review Pollutants Only)

Potential/Fugitive Emissions

1. Pollutant Emitted: NO_x	2. Total Percent Efficiency of Control:
3. Potential Emissions: 362 lb/hour 252 tons/year	4. Synthetically Limited? [X]
5. Range of Estimated Fugitive Emissions: [] 1 [] 2 [] 3 _____ to _____ tons/year	
6. Emission Factor: Reference: GE, 1998; Golder	7. Emissions Method Code: 2
8. Calculation of Emissions (limit to 600 characters): See Attachment PSD-IPS; Section 2.0; Appendix A.	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters): Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,390 hrs/yr gas firing and 1,000 hrs/yr oil firing; ISO conditions.	

Allowable Emissions Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: 9 ppmvd	4. Equivalent Allowable Emissions: 66.7 lb/hour 108.6 tons/year
5. Method of Compliance (limit to 60 characters): CEM - 30 Day Rolling Average	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters): Requested Allowable Emissions and Units is at 15% O2-100% load. Gas firing; 32°F; 100% load, TPY @ 59°F, 3,390 hrs/yr see Attachment PSD-IPS; Section 2.0; Appendix A.	

G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION

(Regulated Emissions Units -

Emissions-Limited and Preconstruction Review Pollutants Only)

Potential/Fugitive Emissions

1. Pollutant Emitted: CO		2. Total Percent Efficiency of Control:	
3. Potential Emissions: 74.4 lb/hour		4. Synthetically Limited? <input checked="" type="checkbox"/> [X] 86.5 tons/year	
5. Range of Estimated Fugitive Emissions: [] 1 [] 2 [] 3 _____ to _____ tons/year			
6. Emission Factor: Reference: GE, 1998; Golder		7. Emissions Method Code: 2	
8. Calculation of Emissions (limit to 600 characters): See Attachment PSD-IPS; Section 2.0; Appendix A.			
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters): Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,390 hrs/yr gas firing and 1,000 hrs/yr oil firing; ISO conditions			

Allowable Emissions Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: OTHER		2. Future Effective Date of Allowable Emissions:	
3. Requested Allowable Emissions and Units: 20 ppmvd		4. Equivalent Allowable Emissions: 74.4 lb/hour 34.7 tons/year	
5. Method of Compliance (limit to 60 characters): EPA Method 10; high and low load			
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters): Oil firing; max @ 32°F; 100% load; TPY @ 59°F, 1,000 hrs/yr. See Attachment PSD-IPS; Section 2.0; Appendix A.			

G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION**(Regulated Emissions Units -****Emissions-Limited and Preconstruction Review Pollutants Only)****Potential/Fugitive Emissions**

1. Pollutant Emitted: CO	2. Total Percent Efficiency of Control:
3. Potential Emissions: 74.4 lb/hour 86.5 tons/year	4. Synthetically Limited? [X]
5. Range of Estimated Fugitive Emissions: [] 1 [] 2 [] 3 _____ to _____ tons/year	
6. Emission Factor: Reference: GE, 1998; Golder	7. Emissions Method Code: 2
8. Calculation of Emissions (limit to 600 characters): See Attachment PSD-IPS; Section 2.0; Appendix A.	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters): Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,390 hrs/yr gas firing and 1,000 hrs/yr oil firing; ISO conditions	

Allowable Emissions Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: 12 ppmvd	4. Equivalent Allowable Emissions: 44.2 lb/hour 72.0 tons/year
5. Method of Compliance (limit to 60 characters): EPA Method 10; high and low load	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters): Gas firing; 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-IPS; Section 2.0; Appendix A.	

G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION
(Regulated Emissions Units -
Emissions-Limited and Preconstruction Review Pollutants Only)

Potential/Fugitive Emissions

1. Pollutant Emitted: VOC	2. Total Percent Efficiency of Control:
3. Potential Emissions: 16.7 lb/hour 11.5 tons/year	4. Synthetically Limited? [X]
5. Range of Estimated Fugitive Emissions: [] 1 [] 2 [] 3 _____ to _____ tons/year	
6. Emission Factor: Reference: GE, 1998; Golder	7. Emissions Method Code: 2
8. Calculation of Emissions (limit to 600 characters): See Attachment PSD-IPS; Section 2.0; Appendix A.	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters): Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,390 hrs/yr gas firing and 1,000 hrs/yr oil firing; ISO conditions	

Allowable Emissions Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: 7 ppmvw	4. Equivalent Allowable Emissions: 16.7 lb/hour 8.1 tons/year
5. Method of Compliance (limit to 60 characters): EPA Method 25A; high and low load	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters): Oil firing; max @ 32°F; 100% load; TPY @ 59°F, 1,000 hrs/yr. See Attachment PSD-IPS; Section 2.0; Appendix A.	

G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION
(Regulated Emissions Units -
Emissions-Limited and Preconstruction Review Pollutants Only)

Potential/Fugitive Emissions

1. Pollutant Emitted: VOC	2. Total Percent Efficiency of Control:
3. Potential Emissions: 16.7 lb/hour 11.5 tons/year	4. Synthetically Limited? [X]
5. Range of Estimated Fugitive Emissions: [] 1 [] 2 [] 3 _____ to _____ tons/year	
6. Emission Factor: Reference: GE, 1998; Golder	7. Emissions Method Code: 2
8. Calculation of Emissions (limit to 600 characters): See Attachment PSD-IPS; Section 2.0; Appendix A.	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters): Lb/hr based on oil firing; 100% load; 32°F. Tons/yr based on 2,390 hrs/yr gas firing and 1,000 hrs/yr oil firing; ISO conditions	

Allowable Emissions Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: 1.4 ppmvd	4. Equivalent Allowable Emissions: 3 lb/hour 4.8 tons/year
5. Method of Compliance (limit to 60 characters): EPA Method 25A; high and low load	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters): Additional requested allowable emissions and units: Gas firing; 32°F; 100% load; TPY @ 59°F, 3,390 hrs/yr. See Attachment PSD-IPS; Section 2.0; Appendix A.	

G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION
(Regulated Emissions Units -
Emissions-Limited and Preconstruction Review Pollutants Only)

Potential/Fugitive Emissions

1. Pollutant Emitted: PM₁₀	2. Total Percent Efficiency of Control:
3. Potential Emissions: 17 lb/hour 20.5 tons/year	4. Synthetically Limited? [X]
5. Range of Estimated Fugitive Emissions: [] 1 [] 2 [] 3 _____ to _____ tons/year	
6. Emission Factor: Reference: GE, 1998; Golder	7. Emissions Method Code: 2
8. Calculation of Emissions (limit to 600 characters): See Attachment PSD-IPS; Section 2.0; Appendix A.	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters): Lb/hr based on oil firing; 100% load; 59°F. Tons/yr based on 2,390 hrs/yr gas firing and 1,000 hrs/yr oil firing; ISO conditions.	

Allowable Emissions Allowable Emissions 1 of 2

1. Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units: 17 lb/hr	4. Equivalent Allowable Emissions: 17 lb/hour 8.5 tons/year
5. Method of Compliance (limit to 60 characters): Annual stack test; EPA Methods 5 or 17; if <400 hours	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters): Oil firing - all loads; 1,000 hrs/yr. See Attachment PSD-IPS; Section 2.0; Appendix A.	

G. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION
(Regulated Emissions Units -
Emissions-Limited and Preconstruction Review Pollutants Only)

Potential/Fugitive Emissions

1. Pollutant Emitted: PM₁₀	2. Total Percent Efficiency of Control:
3. Potential Emissions: 17 lb/hour 20.5 tons/year	4. Synthetically Limited? [X]
5. Range of Estimated Fugitive Emissions: [] 1 [] 2 [] 3 _____ to _____ tons/year	
6. Emission Factor: Reference: GE, 1998; Golder	7. Emissions Method Code: 2
8. Calculation of Emissions (limit to 600 characters): See Attachment PSD-IPS; Section 2.0; Appendix A.	
9. Pollutant Potential/Fugitive Emissions Comment (limit to 200 characters): Lb/hr based on oil firing; 100% load; 59°F. Tons/yr based on 2,390 hrs/yr gas firing and 1,000 hrs/yr oil firing; ISO conditions.	

Allowable Emissions Allowable Emissions 2 of 2

1. Basis for Allowable Emissions Code: OTHER	2. Future Effective Date of Allowable Emissions:
3. Requested Allowable Emissions and Units:	4. Equivalent Allowable Emissions: 10 lb/hour 17.0 tons/year
5. Method of Compliance (limit to 60 characters): VE Test < 20% opacity	
6. Allowable Emissions Comment (Desc. of Operating Method) (limit to 200 characters): Gas firing - all loads; 3,390 hrs/yr. See Attachment PSD-IPS; Section 2.0; Appendix A.	

H. VISIBLE EMISSIONS INFORMATION**(Only Regulated Emissions Units Subject to a VE Limitation)****Visible Emissions Limitation:** Visible Emissions Limitation 1 of 2

1. Visible Emissions Subtype: VE20	2. Basis for Allowable Opacity: [<input checked="" type="checkbox"/>] Rule [<input type="checkbox"/>] Other
3. Requested Allowable Opacity: Normal Conditions: 20 % Exceptional Conditions: % Maximum Period of Excess Opacity Allowed: min/hour	
4. Method of Compliance: Annual VE Test EPA Method 9	
5. Visible Emissions Comment (limit to 200 characters): Maximum for oil firing.	

I. CONTINUOUS MONITOR INFORMATION**(Only Regulated Emissions Units Subject to Continuous Monitoring)****Continuous Monitoring System:** Continuous Monitor 1 of 2

1. Parameter Code: EM	2. Pollutant(s): NO_x
3. CMS Requirement:	[<input checked="" type="checkbox"/>] Rule [<input type="checkbox"/>] Other
4. Monitor Information: Not yet determined Manufacturer: Model Number: Serial Number:	
5. Installation Date: 01 Jan 2002	6. Performance Specification Test Date:
7. Continuous Monitor Comment (limit to 200 characters): NO_x CEM proposed to meet requirements of 40 CFR Part 75.	

J. EMISSIONS UNIT SUPPLEMENTAL INFORMATION
(Regulated Emissions Units Only)**Supplemental Requirements**

1. Process Flow Diagram [X] Attached, Document ID: <u>PSD-IPS</u> [] Not Applicable [] Waiver Requested
2. Fuel Analysis or Specification [X] Attached, Document ID: <u>PSD-IPS</u> [] Not Applicable [] Waiver Requested
3. Detailed Description of Control Equipment [X] Attached, Document ID: <u>PSD-IPS</u> [] Not Applicable [] Waiver Requested
4. Description of Stack Sampling Facilities [X] Attached, Document ID: <u>PSD-IPS</u> [] Not Applicable [] Waiver Requested
5. Compliance Test Report - [] Attached, Document ID: _____ [] Previously submitted, Date: _____ [X] Not Applicable
6. Procedures for Startup and Shutdown [] Attached, Document ID: _____ [X] Not Applicable [] Waiver Requested
7. Operation and Maintenance Plan [] Attached, Document ID: _____ [X] Not Applicable [] Waiver Requested
8. Supplemental Information for Construction Permit Application [X] Attached, Document ID: <u>PSD-IPS</u> [] Not Applicable
9. Other Information Required by Rule or Statute [X] Attached, Document ID: <u>PSD-IPS</u> [] Not Applicable
10. Supplemental Requirements Comment:

Additional Supplemental Requirements for Title V Air Operation Permit Applications**11. Alternative Methods of Operation**☐ Attached, Document ID: _____ ☐ Not Applicable**12. Alternative Modes of Operation (Emissions Trading)**☐ Attached, Document ID: _____ ☐ Not Applicable**13. Identification of Additional Applicable Requirements**☐ Attached, Document ID: _____ ☐ Not Applicable**14. Compliance Assurance Monitoring Plan**☐ Attached, Document ID: _____ ☐ Not Applicable**15. Acid Rain Part Application (Hard-copy Required)**☐ Acid Rain Part - Phase II (Form No. 62-210.900(1)(a))

Attached, Document ID: _____

☐ Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)

Attached, Document ID: _____

☐ New Unit Exemption (Form No. 62-210.900(1)(a)2.)

Attached, Document ID: _____

☐ Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)

Attached, Document ID: _____

☐ Phase II NOx Compliance Plan (Form No. 62-210.900(1)(a)4.)

Attached, Document ID: _____

☐ Phase NOx Averaging Plan (Form No. 62-210.900(1)(a)5.)

Attached, Document ID: _____

☐ Not Applicable

III. EMISSIONS UNIT INFORMATION

A separate Emissions Unit Information Section (including subsections A through J as required) must be completed for each emissions unit addressed in this Application for Air Permit. If submitting the application form in hard copy, indicate, in the space provided at the top of each page, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application.

A. GENERAL EMISSIONS UNIT INFORMATION (All Emissions Units)

Emissions Unit Description and Status

1. Type of Emissions Unit Addressed in This Section: (Check one)			
<input type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).			
<input checked="" type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.			
<input type="checkbox"/> This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only.			
2. Regulated or Unregulated Emissions Unit? (Check one)			
<input type="checkbox"/> The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.			
<input checked="" type="checkbox"/> The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.			
3. Description of Emissions Unit Addressed in This Section (limit to 60 characters):			
Unreg. Emissions Activities - 2 Tanks 2.8 M gallons each			
4. Emissions Unit Identification Number:		<input type="checkbox"/> No ID <input checked="" type="checkbox"/> ID Unknown	
ID:			
5. Emissions Unit Status Code:	6. Initial Startup Date:	7. Emissions Unit Major Group SIC Code:	8. Acid Rain Unit?
C		49	<input type="checkbox"/>
9. Emissions Unit Comment: (Limit to 500 Characters)			
This emission unit information section addresses two 2.8 million gallon tanks as unregulated emission units. NSPS Subpart Kb recordkeeping requirements are applicable; there is no emission limiting or work practice standards. See Attachment PSD-IPS.			

Emissions Unit Control Equipment

1. Control Equipment/Method Description (Limit to 200 characters per device or method):

2. Control Device or Method Code(s):

Emissions Unit Details

1. Package Unit:	
Manufacturer:	Model Number:
2. Generator Nameplate Rating: MW	
3. Incinerator Information:	
Dwell Temperature:	°F
Dwell Time:	seconds
Incinerator Afterburner Temperature:	°F

E. SEGMENT (PROCESS/FUEL) INFORMATION
(All Emissions Units)**Segment Description and Rate:** Segment 1 of 1

1. Segment Description (Process/Fuel Type) (limit to 500 characters): No. 2 Distillate Oil/Diesel		
2. Source Classification Code (SCC): A2505030090		3. SCC Units: 1,000 gallons used
4. Maximum Hourly Rate:	5. Maximum Annual Rate: 55,600	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur:	8. Maximum % Ash:	9. Million Btu per SCC Unit: 131.8
10. Segment Comment (limit to 200 characters): Annual rate combined for both tanks based on inputs to CTs; 18,560 Btu/lb (LHV); and 7.1 lb/gal at 59°F.		

Segment Description and Rate: Segment ____ of ____

1. Segment Description (Process/Fuel Type) (limit to 500 characters): 		
2. Source Classification Code (SCC):		3. SCC Units:
4. Maximum Hourly Rate:	5. Maximum Annual Rate:	6. Estimated Annual Activity Factor:
7. Maximum % Sulfur:	8. Maximum % Ash:	9. Million Btu per SCC Unit:
10. Segment Comment (limit to 200 characters): 		

F. EMISSIONS UNIT POLLUTANTS
(All Emissions Units)

1. Pollutant Emitted	2. Primary Control Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
VOC			NS

PART B

REPORT

1.0 INTRODUCTION

IPS Avon Park Corporation proposes to license, construct, and operate a nominal 680-megawatt (MW) independent power production facility, referred to as the IPS Vandolah Power Project, in an unincorporated area of Hardee County, Florida (Figure 1-1). The site will be located on an about 20-acre tract near Vandolah, Florida. The project consists of four 170-MW dual-fuel, General Electric Frame 7FA combustion turbines (CTs) that will use dry low-nitrogen oxide (NO_x) (DLN) combustion technology when operating on natural gas and water injection (for NO_x control) when operating on distillate fuel oil. The facility is designed for peaking service. The primary fuel for the combustion turbines will be natural gas with distillate fuel oil used as backup fuel. Fuel oil will contain a maximum sulfur content of 0.05 percent.

The permitting of the project in Florida requires an air construction permit and prevention of significant deterioration (PSD) review approval. To assist in performing the necessary licensing activities, IPS Avon Park Corporation has contracted Golder Associates Inc. (Golder) to perform the necessary air quality assessments for determining the project's compliance with state and federal new source review (NSR) regulation, including PSD and nonattainment review requirements. The critical aspects of these assessments include the air quality impact analyses performed using an air dispersion model and the best available control technology (BACT) analyses performed to evaluate the selected emission control technology.

The proposed project will be a new air pollution source that will result in increases in air emissions in Hardee County. The U.S. Environmental Protection Agency (EPA) has implemented regulations requiring a PSD review. PSD regulations are promulgated under 10 Code of Federal Regulations (CFR) Part 52.21 and implemented through delegation to the Florida Department of Environmental Protection (DEP). Florida's PSD regulations are codified in Rules 62-212.400, F.A.C. These regulations incorporate the EPA PSD regulations.

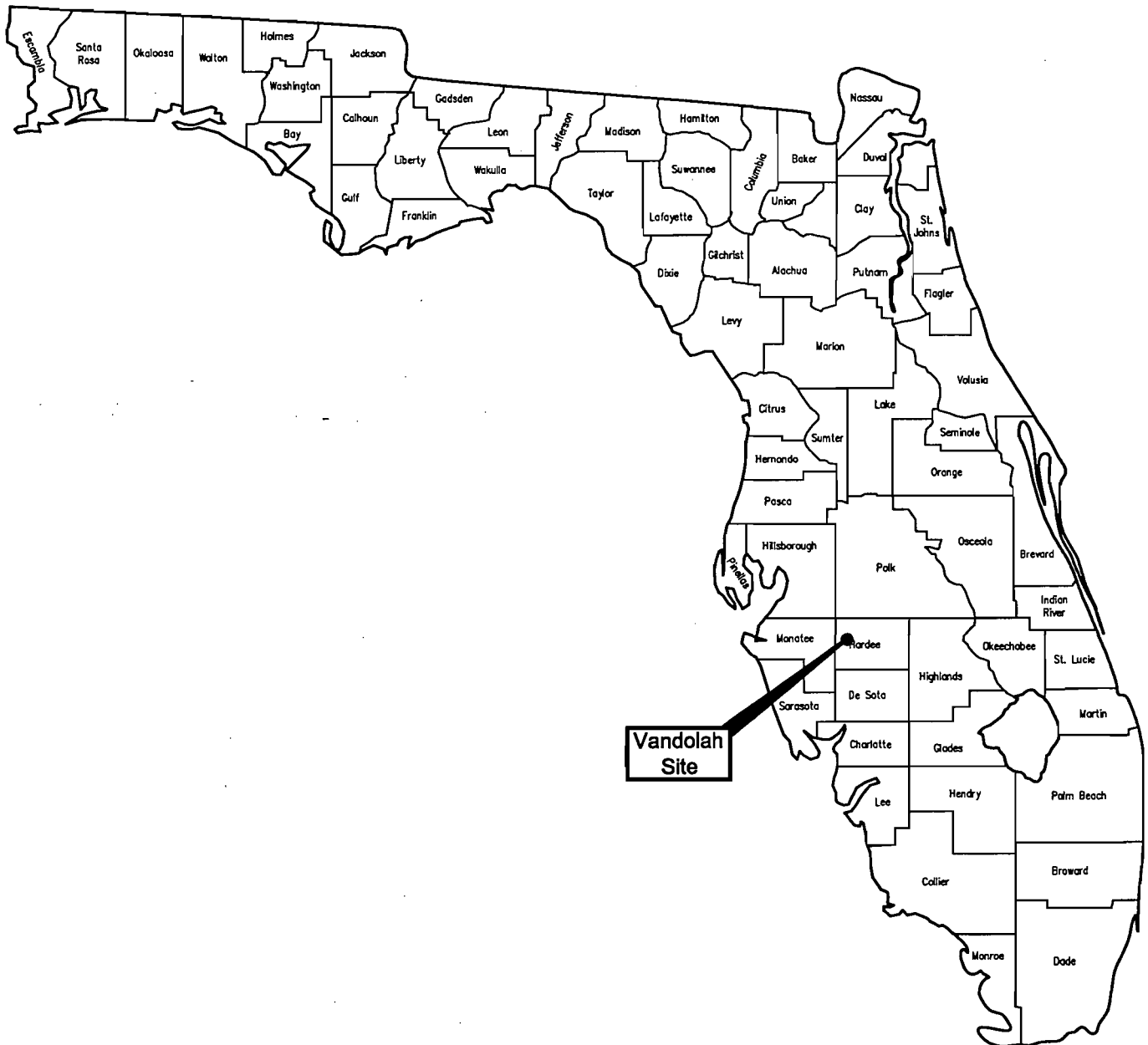
Based on the emissions from the proposed project, a PSD review is required for each of the following regulated pollutants:

- Particulate matter (PM) as total suspended particulate matter (TSP),
- Particulate matter with aerodynamic diameter of 10 microns or less (PM₁₀),
- Nitrogen dioxide (NO₂),
- Sulfur dioxide (SO₂),
- Carbon monoxide (CO), and
- Volatile organic compounds (VOC).

Hardee County has been designated as an attainment or unclassifiable area for all criteria pollutants [i.e., attainment: ozone (O₃), PM₁₀, SO₂, CO, and NO₂; unclassifiable: lead] and is classified as a PSD Class II area for PM₁₀, SO₂, and NO₂; therefore, the PSD review will follow regulations pertaining to such designations.

The air permit application is divided into seven major sections.

- Section 2.0 presents a description of the facility, including air emissions and stack parameters.
- Section 3.0 provides a review of the PSD and nonattainment requirements applicable to the proposed project.
- Section 4.0 includes the control technology review with discussions on BACT.
- Section 5.0 discusses the ambient air monitoring analysis (pre-construction monitoring) required by PSD regulations.
- Section 6.0 presents a summary of the air modeling approach and results used in assessing compliance of the proposed project with ambient air quality standards (AAQS), PSD increments, and good engineering practice (GEP) stack height regulations.
- Section 7.0 provides the additional impact analyses for soils, vegetation, and visibility.



JOB No.: 993-9551	SCALE: NTS
CAD BY: CDT	DATE: 7/26/99
CHK BY:	FILE No.: gen-loc-1-1.dwg
REV BY:	DR SUBTITLE: —

Golder Associates

General Location of IPS
Vandolah Power Project

IPS Avon Park Corp.

FIGURE 1-1

2.0 PROJECT DESCRIPTION

2.1 SITE DESCRIPTION

The project site, shown in Figure 2-1, consists of about 20 acres that are currently agricultural. There is minimal industrial, commercial, and residential development within a 3-km radius of the site. The plant elevation will be approximately 100 feet above sea level. The terrain surrounding the site is flat.

Natural gas will be supplied by a lateral pipeline connected to the Florida Gas Transmission (FGT) natural gas pipeline located north of the site. The site has access to transmission facilities from a 230 kV transmission line and electrical substation that is located to the west of the site. Water for the evaporative cooler, and NO_x control when firing oil, will be supplied by nearby groundwater or surface water sources. Potable water and additional fire protection supply water will be served from groundwater wells.

2.2 POWER PLANT

The proposed project will consist of four General Electric Frame 7FA CTs and associated facilities. The annual maximum capacity factor of the plant will be 39 percent, which is equivalent to operating 3,390 hours/year at full load. Natural gas will be used as the primary fuel, and fuel oil will be used as a backup fuel. Fuel oil usage will be limited to the equivalent of 1,000 hours/year at full load.

Plant performance with General Electric 7FA combustion turbines was developed for natural gas and oil; at 50-, 75-, and 100-percent load; and at 32°F, 59°F, and 95°F turbine inlet temperatures. Combustion turbine performance is based on a performance envelope developed from General Electric and has been adjusted to reflect degradation and performance improvements. In particular, the combustion turbine emission estimates accounts for 5 percent higher power output and a 6 percent degradation (see Appendix A). This 11 percent was used to increase mass flow of the turbine.

The CTs will be capable of operating from 50 to 100 percent of baseload. The efficiency of the CTs decreases at part load. As a result, the economic incentive is to dispatch the plant to keep the units operating as near baseload as possible.

Natural gas will be transported to the site via pipeline and fuel oil will be trucked to the site. The distillate fuel oil, which will have a maximum sulfur content of 0.05 percent, will be stored onsite in two aboveground storage tanks, each sized to hold approximately 67,000 barrels (2.8 million gallons).

Air emissions control will consist of using state-of-the-art dry low- NO_x burners in the CTs when firing natural gas. The General Electric Frame 7FA will be equipped with the General Electric dry low- 2.6 (DLN- NO_x) combustion system that regulates the distribution of fuel delivery to a multi-nozzle, total premix combustor arrangement. The fuel flow distribution to each combustion system fuel nozzle is regulated to maintain unit load and optimum turbine emissions. The DLN-2.6 combustion system consists of six fuel nozzles per combustion can, with each operating as a fully premixed combustor. Of the six nozzles, five are located radially and one is in the center. The fuel system is fully automated and sequences the DLN-2.6 combustion system through a number of staging modes prior to reaching full load. The General Electric Frame 7FA has 14 combustors per turbine. Water injection will be used for NO_x control when firing distillate fuel oil. The SO_2 emissions will be controlled by the use of low-sulfur fuels. Good combustion practices and clean fuels will also minimize potential emissions of PM, CO, VOC, and other pollutants (e.g., trace metals). These engineering and environmental designs maximize control of air emissions while minimizing economic, environmental, and energy impacts (see Section 4.0 for the BACT evaluation).

2.3 PROPOSED SOURCE EMISSIONS AND STACK PARAMETERS

The estimated maximum hourly emissions and exhaust information representative of the proposed CT design operating at baseload conditions (100-percent load), 75-percent load and 50-percent load conditions are presented in Tables 2-1 through 2-6. The information is presented in these tables for one unit simple cycle operation based on natural gas combustion and fuel oil combustion. The data are presented for turbine inlet temperatures of 32°F, 59°F,

and 95°F. These temperatures represent the range of ambient temperatures that the CTs are most likely to experience.

The performance calculations for the operating conditions are given in Appendix A.

The pollutant gaseous emission concentrations and PM₁₀ emission rates for the proposed CTs are as follows:

Pollutant	Natural Gas	Distillate Oil
NO _x , ppmvd @ 15% O ₂	9	42
CO, ppmvd (ppmvd @ 15% O ₂)	12 (16)	20
VOC as CH ₄ , ppmvd (gas), ppmvw (oil)	1.44 (32)	7
SO _x as SO ₂	Calculated Based on Fuel (1.0 grains S/100 SCF)	Calculated Based on Fuel (0.05% sulfur)
PM ₁₀ lb/hr (dry filterable)	10	17

The maximum short-term emission rates (lb/hr) generally occur at baseload, 32°F operation, where the CT has the greatest output and greatest fuel consumption.

Based on a turbine inlet temperature of 59°F, the emission rates used to calculate maximum potential annual emissions for the proposed facility for regulated air pollutants are presented in Table 2-7 for 1 and 4 CTs. To produce the maximum annual emissions, the CTs are assumed to operate at baseload for 3,390 hours (39 percent capacity factor) firing natural gas for 2,390 hours and fuel oil for 1,000 hours. The potential emissions are based on the 59°F turbine inlet air condition since it represents a nominal average between the higher emission levels at the 32°F turbine inlet condition (winter) and the infrequent 95°F turbine inlet condition (summer).

Process flow diagrams of the turbine operating at turbine inlet temperature of 95°F, 59°F, and 32°F are presented in Figures 2-2 and 2-4, respectively for the "F" Class CT.

Based on a review of the emission rates for natural gas and fuel oil combustion, the highest emission rates for the regulated pollutants generally occur when firing fuel oil. Combustion of natural gas and fuel oil result in slightly different exhaust flow gas rates and stack exit

temperatures; however, the differences are minor. As a result of the higher emissions when firing oil, the air modeling analyses were based on determining maximum ground-level impacts with fuel oil.

As discussed in Section 6.0, the air modeling analyses that addressed compliance with ambient standards were based on modeling the CTs for the operating load and ambient temperature which produced the maximum impacts from the load impact analysis that was performed. Although the highest emission rates occur with low turbine inlet temperatures (i.e., 32°F) and baseload conditions, the lowest exhaust gas flow rates occur with a turbine inlet temperature of 95°F and 50 percent operating load. Since this low exhaust flow condition can result in potentially higher impacts due to lower plume rise (i.e., due to lower exit velocity and temperature), the load analysis included modeling the CTs for the following four scenarios designed to determine the maximum impacts for the project:

- Base operating load for the turbine inlet temperature of 32°F;
- Base operating load for the turbine inlet temperature of 95°F;
- A 50-percent operating load for the turbine inlet temperature of 32°F; and
- A 50-percent operating load for the turbine inlet temperature of 95°F.

2.4 SITE LAYOUT, STRUCTURES, AND STACK SAMPLING FACILITIES

Plot plan of the proposed facility is presented in Figure 2-5. The dimensions of the buildings and structures are presented in Section 6.0. Stack sampling facilities will be constructed in accordance to Rule 62-297.310(6) F.A.C.

Table 2-1. Stack, Operating, and Emission Data for the Proposed GE 7FA Combustion Turbine with Dry Low-NO_x Combustors Firing Natural Gas-- Baseload for Simple Cycle Operation

Dry Low NO _x Combustors Firing Natural Gas - Baseline for Example 1 of the Emission				
Parameter		Operating and Emission Data ^a for Ambient Temperature		
		32°F	59°F	95°F
<u>Stack Data (ft)</u>				
Height		60	60	60
Diameter		22	22	22
<u>Operating Data</u>				
Temperature (°F)		1,097	1,113	1,135
Velocity (ft/sec)		118.7	116.0	111.1
<u>Maximum Hourly Emission per Unit^b</u>				
SO ₂	lb/hr	5.1	5.0	4.6
	Basis	1.0 grain S/100CF	1.0 grain S/100CF	1.0 grain S/100CF
PM/PM10	lb/hr	10	10	10
	Basis	Dry filterables	Dry filterables	Dry filterables
NO _x	lb/hr	66.7	64.1	59.9
	Basis	9 ppmvd at 15% O ₂	9 ppmvd at 15% O ₂	9 ppmvd at 15% O ₂
CO	lb/hr	44.2	42.5	39.3
	Basis	12 ppmvd	12 ppmvd	12 ppmvd
VOC (as methane)	lb/hr	2.95	2.83	2.62
	Basis	1.4 ppmvd	1.4 ppmvd	1.4 ppmvd

Note: ppmvd = parts per million volume dry; O₂ = oxygen; S = sulfur; CF = cubic feet

^a Refer to Appendix A for detailed information.

^b Other regulated pollutants are assumed to have negligible emissions. These pollutants include lead, reduced sulfur compounds, hydrogen sulfide, fluorides, beryllium, mercury, arsenic, asbestos, vinyl chloride, and radionuclides.

Table 2-2. Stack, Operating, and Emission Data for the Proposed GE 7FA Combustion Turbine with Dry Low-NO_x Combustors Firing Natural Gas-- 75 Percent Load for Simple Cycle Operation

Parameter	Operating and Emission Data ^a for Ambient Temperature			
	32°F	59°F	95°F	
<u>Stack Data (ft)</u>				
Height	60	60	60	
Diameter	22	22	22	
<u>Operating Data</u>				
Temperature (°F)	1,170	1,179	1,193	
Velocity (ft/sec)	100.5	98.2	95.0	
<u>Maximum Hourly Emission per Unit^b</u>				
SO ₂	lb/hr	4.2	4.0	3.7
	Basis	1.0 grain S/100CF	1.0 grain S/100CF	1.0 grain S/100CF
PM/PM10	lb/hr	10	10	10
	Basis	Dry filterables	Dry filterables	Dry filterables
NO _x	lb/hr	54.4	52.4	48.3
	Basis	9 ppmvd at 15% O ₂	9 ppmvd at 15% O ₂	9 ppmvd at 15% O ₂
CO	lb/hr	35.7	34.6	32.7
	Basis	12 ppmvd	12 ppmvd	12 ppmvd
VOC (as methane)	lb/hr	2.38	2.31	2.18
	Basis	1.4 ppmvd	1.4 ppmvd	1.4 ppmvd

Note: ppmvd = parts per million volume dry; O₂ = oxygen; S = sulfur; CF = cubic feet

^a Refer to Appendix A for detailed information.

^b Other regulated pollutants are assumed to have negligible emissions. These pollutants include lead, reduced sulfur compounds, hydrogen sulfide, fluorides, beryllium, mercury, arsenic, asbestos, vinyl chloride, and radionuclides.

Table 2-3. Stack, Operating, and Emission Data for the Proposed GE 7FA Combustion Turbine with Dry Low-NO_x Combustors Firing Natural Gas-- 50 Percent Load for Simple Cycle Operation

		Operating and Emission Data ^a for Ambient Temperature		
Parameter		32°F	59°F	95°F
<u>Stack Data (ft)</u>				
Height		60	60	60
Diameter		22	22	22
<u>Operating Data</u>				
Temperature (°F)		1,171	1,186	1,200
Velocity (ft/sec)		84.2	82.0	80.5
<u>Maximum Hourly Emission per Unit^b</u>				
SO ₂	lb/hr	3.4	3.2	2.9
	Basis	1.0 grain S/100CF	1.0 grain S/100CF	1.0 grain S/100CF
PM/PM10	lb/hr	10	10	10
	Basis	Dry filterables	Dry filterables	Dry filterables
NO _x	lb/hr	43.4	40.8	38.3
	Basis	9 ppmvd at 15% O ₂	9 ppmvd at 15% O ₂	9 ppmvd at 15% O ₂
CO	lb/hr	30.0	28.9	27.8
	Basis	12 ppmvd	12 ppmvd	12 ppmvd
VOC (as methane)	lb/hr	2.00	1.90	1.85
	Basis	1.4 ppmvd	1.4 ppmvd	1.4 ppmvd

Note: ppmvd = parts per million volume dry; O₂ = oxygen; S = sulfur; CF = cubic feet

^a Refer to Appendix A for detailed information.

^b Other regulated pollutants are assumed to have negligible emissions. These pollutants include lead, reduced sulfur compounds, hydrogen sulfide, fluorides, beryllium, mercury, arsenic, asbestos, vinyl chloride, and radionuclides.

Table 2-4. Stack, Operating, and Emission Data for the Proposed GE 7FA Combustion Turbine with Water Injection Firing Distillate Fuel Oil-- Baseload for Simple Cycle Operation

Parameter	Operating and Emission Data ^a for Ambient Temperature			
	32°F	59°F	95°F	
<u>Stack Data (ft)</u>				
Height	60	60	60	
Diameter	22	22	22	
<u>Operating Data</u>				
Temperature (°F)	1,076	1,094	1,121	
Velocity (ft/sec)	122.4	119.7	115.0	
<u>Maximum Hourly Emission per Unit^b</u>				
SO ₂	lb/hr	101.5	98.7	93.4
	Basis	0.05 % S	0.05 % S	0.05 % S
PM/PM10	lb/hr	17.0	17.0	17.0
	Basis	Dry filterables	Dry filterables	Dry filterables
NO _x	lb/hr	362.0	350.8	335.8
	Basis	42 ppmvd at 15% O ₂	42 ppmvd at 15% O ₂	42 ppmvd at 15% O ₂
CO	lb/hr	74.4	71.4	66.2
	Basis	20 ppmvd	20.3 ppmvd	20.2 ppmvd
VOC (as methane)	lb/hr	16.7	16.2	15.3
	Basis	7 ppmvw	7 ppmvw	7 ppmvw

Note: ppmvd = parts per million volume dry; O₂ = oxygen; S = sulfur; CF = cubic feet; ppmvw = parts per million volume wet

^a Refer to Appendix A for detailed information.

^b Other regulated pollutants are assumed to have negligible emissions. These pollutants include lead, reduced sulfur compounds, hydrogen sulfide, fluorides, beryllium, mercury, arsenic, asbestos, vinyl chloride, and radionuclides.

Table 2-5. Stack, Operating, and Emission Data for the Proposed GE 7FA Combustion Turbine with Water Injection Firing Distillate Fuel Oil-- 75 Percent Load for Simple Cycle Operation

Parameter	Operating and Emission Data ^a for Ambient Temperature			
	32°F	59°F	95°F	
<u>Stack Data (ft)</u>				
Height	60	60	60	
Diameter	22	22	22	
<u>Operating Data</u>				
Temperature (°F)	1,170	1,176	1,186	
Velocity (ft/sec)	101.0	99.6	97.0	
<u>Maximum Hourly Emission per Unit^b</u>				
SO ₂	lb/hr	82.6	80.1	74.8
	Basis	0.05 % S	0.05 % S	0.05 % S
PM/PM10	lb/hr	17	17	17
	Basis	Dry filterables	Dry filterables	Dry filterables
NO _x	lb/hr	296.7	285.0	267.8
	Basis	42 ppmvd at 15% O ₂	42 ppmvd at 15% O ₂	42 ppmvd at 15% O ₂
CO	lb/hr	57.6	56.4	53.9
	Basis	20 ppmvd	20 ppmvd	20 ppmvd
VOC (as methane)	lb/hr	13.0	12.8	12.4
	Basis	7 ppmvw	5.4 ppmvw	5.5 ppmvw
Sulfuric Acid Mist	lb/hr	13.8	13.0	11.9
	Basis	10% SO ₂	10% SO ₂	10% SO ₂

Note: ppmvd = parts per million volume dry; O₂ = oxygen; S = sulfur; CF = cubic feet; ppmvw = parts per million volume wet

^a Refer to Appendix A for detailed information.

^b Other regulated pollutants are assumed to have negligible emissions. These pollutants include lead, reduced sulfur compounds, hydrogen sulfide, fluorides, beryllium, mercury, arsenic, asbestos, vinyl chloride, and radionuclides.

Table 2-6. Stack, Operating, and Emission Data for the Proposed GE 7FA Combustion Turbine with Water Injection Firing Distillate Fuel Oil-- 50 Percent Load for Simple Cycle Operation

Parameter	Operating and Emission Data ^a for Ambient Temperature			
	32°F	59°F	95°F	
<u>Stack Data (ft)</u>				
Height	60	60	60	
Diameter	22	22	22	
<u>Operating Data</u>				
Temperature (°F)	1,200	1,200	1,200	
Velocity (ft/sec)	85.7	83.3	81.5	
<u>Maximum Hourly Emission per Unit^b</u>				
SO ₂	lb/hr	65.6	62.8	58.9
	Basis	0.05 % S	0.05 % S	0.05 % S
PM/PM10	lb/hr	17	17	17
	Basis	Dry filterables	Dry filterables	Dry filterables
NO _x	lb/hr	236.4	224.0	209.3
	Basis	42 ppmvd at 15% O ₂	42 ppmvd at 15% O ₂	42 ppmvd at 15% O ₂
CO	lb/hr	72.2	69.8	67.5
	Basis	30 ppmvd	30 ppmvd	30 ppmvd
VOC (as methane)	lb/hr	10.8	10.5	10.3
	Basis	7 ppmvw	7 ppmvw	7 ppmvw

Note: ppmvd = parts per million volume dry; O₂ = oxygen; S = sulfur; CF = cubic feet; ppmvw = parts per million volume wet

^a Refer to Appendix A for detailed information.

^b Other regulated pollutants are assumed to have negligible emissions. These pollutants include lead, reduced sulfur compounds, hydrogen sulfide, fluorides, beryllium, mercury, arsenic, asbestos, vinyl chloride, and radionuclides.

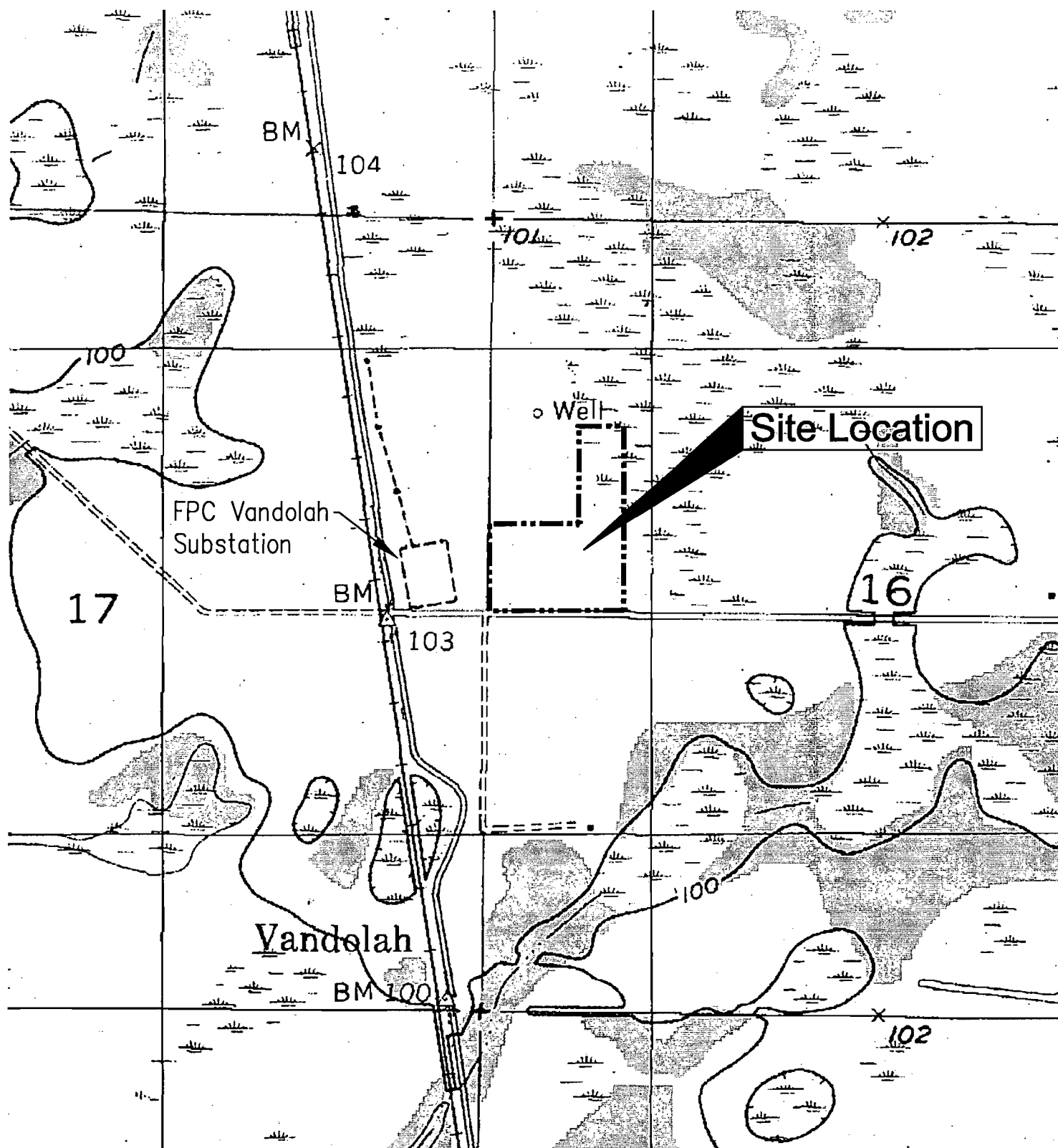
Table 2-7. Maximum Potential Emissions for the IPS Vandolah Power Project - Tons/Year

Natural Gas Firing ^a					Distillate Oil Firing ^b				Maximum
Pollutant	Units	Load at 59 °F Turbine Inlet			Units	Load at 59 °F Turbine Inlet			Emissions w/ oil-firing ^c
		100%	75%	50%		100%	75%	50%	
PM	1	17.0	17.0	17.0	1	8.5	8.5	8.5	20.5
SO ₂	1	8.4	6.8	5.4	1	49.3	40.0	31.4	55.3
NO _x	1	108.6	88.8	69.2	1	175.4	142.6	112.0	252.0
CO	1	72.0	58.6	49.0	1	35.7	28.2	34.9	86.5
VOC	1	4.8	3.9	3.3	1	8.1	6.4	5.3	11.5
PM	4	67.8	67.8	67.8	4	34.0	34.0	34.0	81.8
SO ₂	4	33.6	27.4	21.6	4	197.4	160.1	125.6	221.1
NO _x	4	434.4	355.3	276.8	4	701.6	570.5	448.1	1007.8
CO	4	287.9	234.5	195.8	4	142.9	112.7	139.6	345.9
VOC	4	19.2	15.6	13.1	4	32.4	25.6	21.1	45.9

Notes: ^a 3,390 hours per year operation.

^b 1,000 hours per year operation.

^c 2,390 hours of gas firing and 1,000 hours of oil firing.



REFERENCE

USGS 7.5 Minute Topographic Quadrangle Map, Ft. Green, Florida

0 250' 500' 1000'
SCALE: 1" = 1000'



JOB No.:	993-9551	SCALE:	As Noted
DRAWN BY:	CDT	DATE:	8/26/99
CHECK BY:		FILE No.:	hardee-site-3-1.dwg
REV BY:		DR SUBTITLE:	-

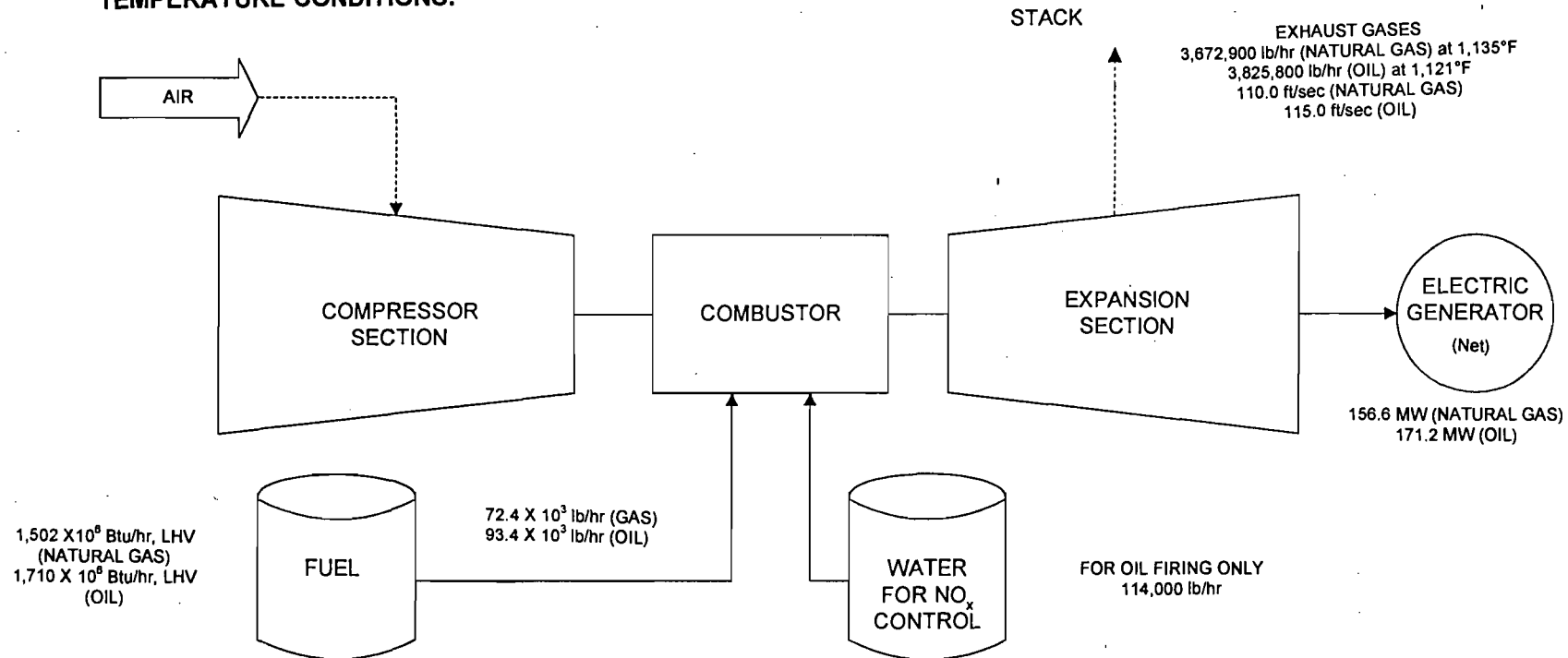
IPS Vandolah Power Project Site Topographic Map

Golder Associates

IPS Avon Park Corp.

FIGURE 2-1

**95°F TURBINE INLET
TEMPERATURE CONDITIONS:**



NOTE: SEE APPENDIX A FOR DESIGN INFORMATION AND STACK PARAMETERS FOR EACH FUEL.

2-13

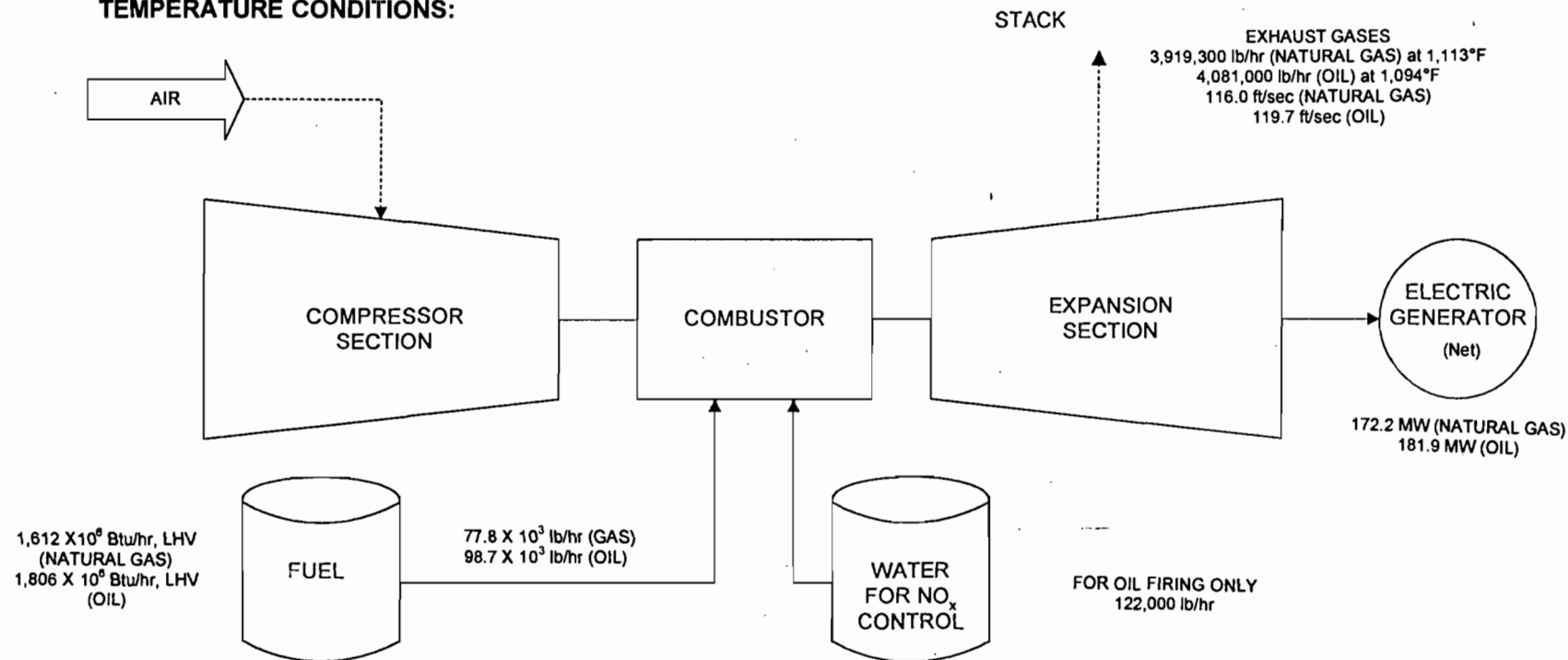
Figure 2-2
Simplified Flow Diagram of Proposed "F" Class
Combustion Turbine
Baseload, Summer Design Conditions

Process Flow Legend
 Solid/Liquid —————→
 Gas - - - - -→
 Steam ·········→

Filename: TO-KAH/FIGURE.VSD
Date: 10/13/98



**59°F TURBINE INLET
TEMPERATURE CONDITIONS:**



NOTE: SEE APPENDIX A FOR DESIGN INFORMATION AND STACK PARAMETERS FOR EACH FUEL.

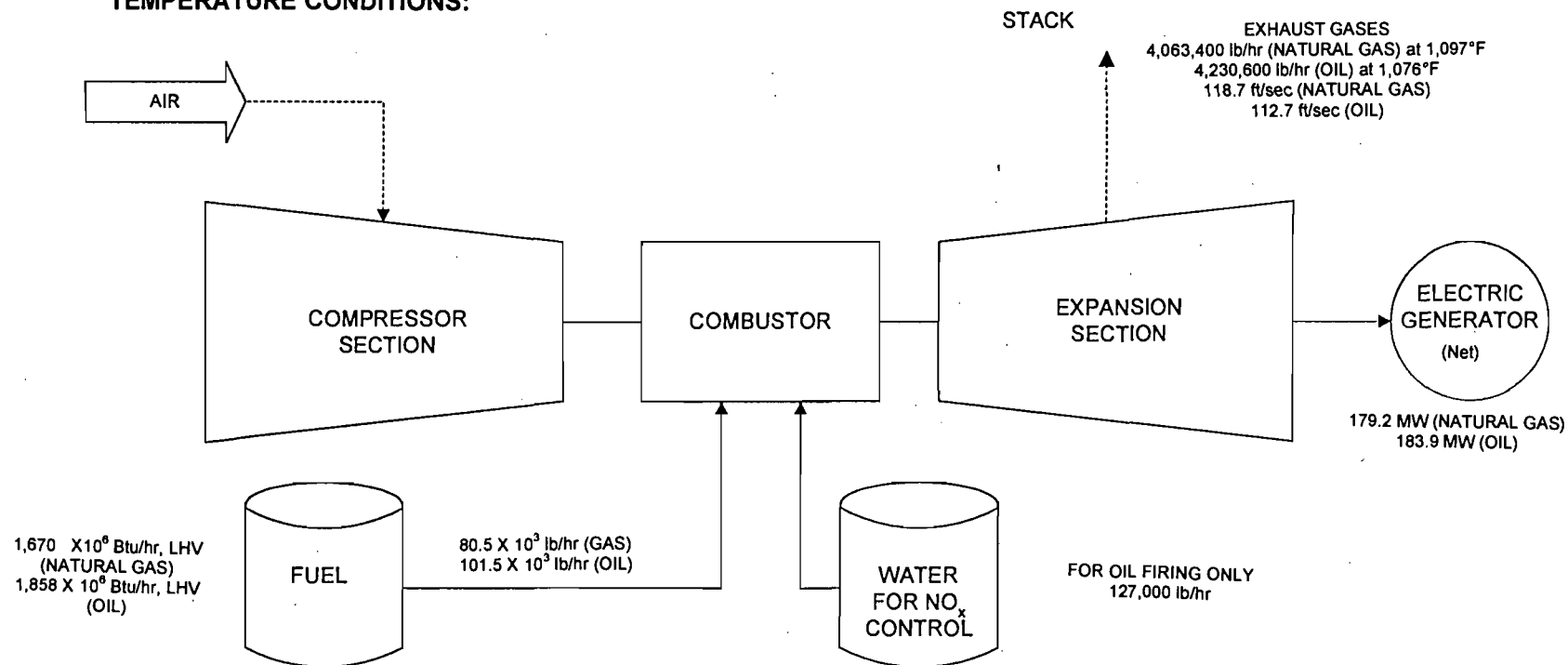
Figure 2-3
Simplified Flow Diagram of Proposed "F" Class
Combustion Turbine
Baseload, Annual Design Conditions

Process Flow Legend	
Solid/Liquid	—————→
Gas	- - - - -→
Steam	· · · · ·→

Filename: TO-KAH/FIGURE.VSD
Date: 10/13/98



**32°F TURBINE INLET
TEMPERATURE CONDITIONS:**



NOTE: SEE APPENDIX A FOR DESIGN INFORMATION AND STACK PARAMETERS FOR EACH FUEL.

Figure 2-4
Simplified Flow Diagram of Proposed "F" Class
Combustion Turbine
Baseload, Winter Design Conditions

Process Flow Legend

Solid/Liquid ———→

Gas - - - - -→

Steam ······→

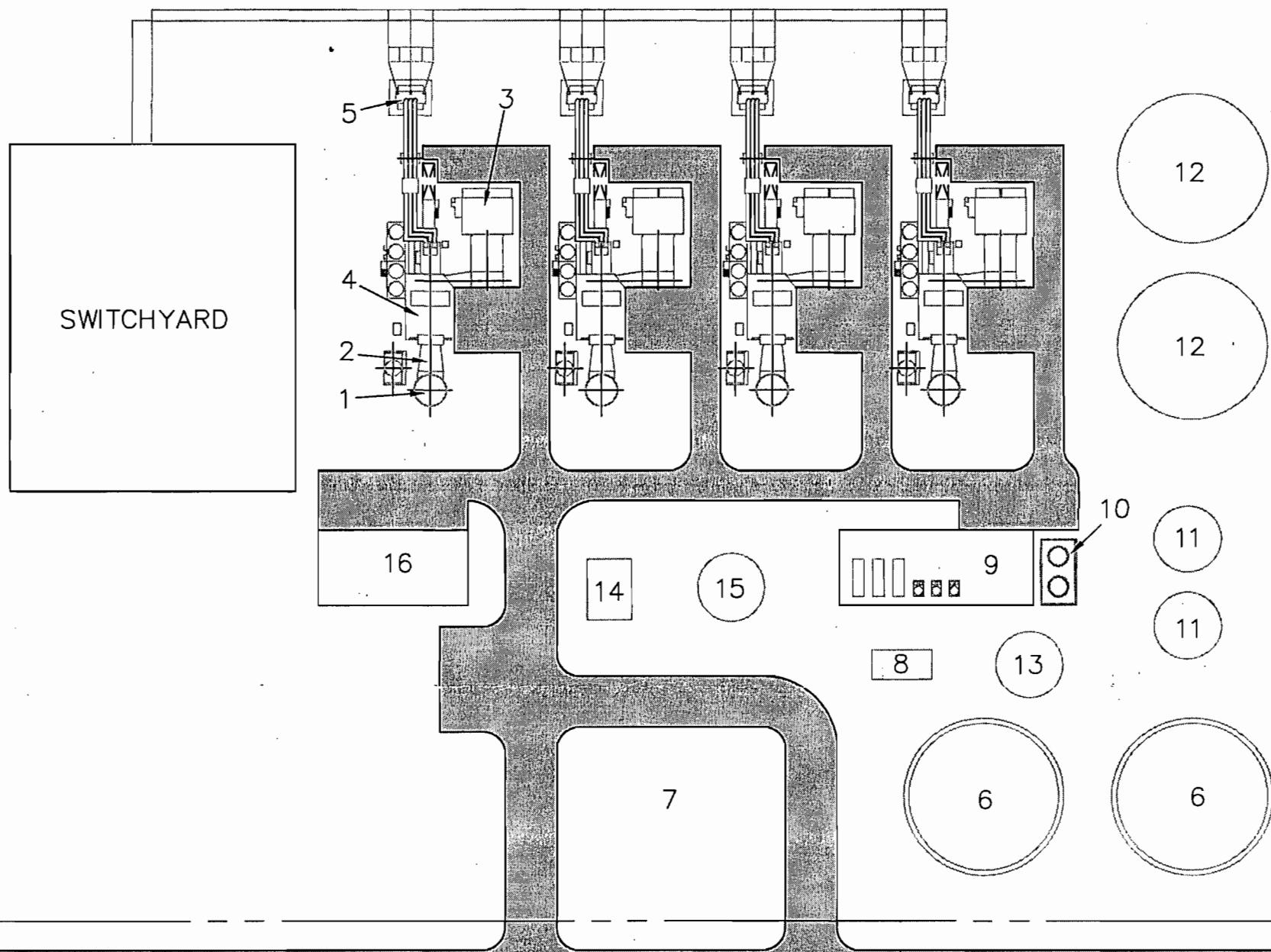
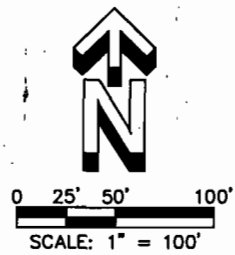
Filename: TO-KAH/FIGURE.VSD

Date: 10/13/98



LIST OF MAJOR COMPONENTS

- 1 STACK
- 2 COMBUSTION TURBINE
- 3 INLET AIR FILTER
- 4 GENERATOR
- 5 TRANSFORMER
- 6 FUEL OIL STORAGE TANKS
- 7 FUEL UNLOADING AREA
- 8 OIL / WATER SEPARATOR
- 9 WATER TREATMENT
- 10 CHEMICAL STORAGE
- 11 RAW / TREATED WATER TANKS
- 12 DEMINERALIZED WATER TANKS
- 13 WASTEWATER TANK
- 14 FIRE PROTECTION PUMP
- 15 FIRE PROTECTION TANK
- 16 OPERATION / MAINTENANCE BUILDING



JOB No.:	993-9558	SCALE:	As Shown
CAD BY:	CDT	DATE:	8/27/99
CHK BY:	KFK	FILE No.:	site.dwg
REV BY:	KFK	DR SUBTITLE:	

Golder Associates

Preliminary Site Plan

IPS Avon Park Corp.

3.0 AIR QUALITY REVIEW REQUIREMENTS AND APPLICABILITY

The following discussion pertains to the federal and state air regulatory requirements and their applicability to the proposed IPS Vandolah Power Project. These regulations must be satisfied before the proposed project can begin operation.

3.1 NATIONAL AND STATE AAQS

The existing applicable national and Florida AAQS are presented in Table 3-1. Primary national AAQS were promulgated to protect the public health, and secondary national AAQS were promulgated to protect the public welfare from any known or anticipated adverse effects associated with the presence of pollutants in the ambient air. Areas of the country in violation of AAQS are designated as nonattainment areas, and new sources to be located in or near these areas may be subject to more stringent air permitting requirements.

3.2 PSD REQUIREMENTS

3.2.1 GENERAL REQUIREMENTS

Under federal and State of Florida PSD review requirements, all major new or modified sources of air pollutants regulated under the Clean Air Act (CAA) must be reviewed and a pre-construction permit issued. Florida's State Implementation Plan (SIP), which contains PSD regulations, has been approved by EPA; therefore, PSD approval authority has been granted to DEP.

A "major facility" is defined as any one of 28 named source categories that have the potential to emit 100 tons per year (TPY) or more or any other stationary facility that has the potential to emit 250 TPY or more of any pollutant regulated under CAA. "Potential to emit" means the capability, at maximum design capacity, to emit a pollutant after the application of control equipment.

A "major modification" is defined under PSD regulations as a change at an existing major facility that increases emissions by greater than significant amounts. PSD significant emission rates are shown in Table 3-2.

EPA has promulgated as regulations certain increases above an air quality baseline concentration level of SO₂, PM₁₀, and NO₂ concentrations that would constitute significant deterioration. The EPA class designations and allowable PSD increments are presented in Table 3-1. The State of Florida has adopted the EPA class designations and allowable PSD increments for SO₂, PM₁₀, and NO₂ increments.

PSD review is used to determine whether significant air quality deterioration will result from the new or modified facility. Federal PSD requirements are contained in 40 CFR 52.21, Prevention of Significant Deterioration of Air Quality. The State of Florida has adopted PSD regulations by reference [Rule 62-212.400 F.A.C.]. Major facilities and major modifications are required to undergo the following analysis related to PSD for each pollutant emitted in significant amounts:

1. Control technology review,
2. Source impact analysis,
3. Air quality analysis (monitoring),
4. Source information, and
5. Additional impact analyses.

In addition to these analyses, a new facility also must be reviewed with respect to GEP stack height regulations. Discussions concerning each of these requirements are presented in the following sections.

3.2.2 CONTROL TECHNOLOGY REVIEW

The control technology review requirements of the federal and state PSD regulations require that all applicable federal and state emission-limiting standards be met, and that BACT be applied to control emissions from the source (Rule 62-212.410, F.A.C.). The BACT requirements are applicable to all regulated pollutants for which the increase in emissions from the facility or modification exceeds the significant emission rate (see Table 3-2).

BACT is defined in 52.21 (b)(12) and Rule 62-210.200(40), F.A.C., as:

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An emissions limitation (including a visible emission standard) based on the maximum degree of reduction of each pollutant subject to regulation under the Act which would be emitted by any proposed major stationary source or major modification which the Administrator, on a case-by-case basis, taking into account energy, environmental, and economic impacts, and other costs, determines is achievable through application of production processes and available methods, systems, and techniques (including fuel cleaning or treatment or innovative fuel combustion techniques) for control of such pollutant. In no event shall application of best available control technology result in emissions of any pollutant which would exceed the emissions allowed by any applicable standard under 40 CFR Parts 60 and 61. If the Administrator determines that technological or economic limitations on the application of measurement methodology to a particular part of a source or facility would make the imposition of an emission standard infeasible, a design, equipment, work practice, operational standard or combination thereof, may be prescribed instead to satisfy the requirement for the application of BACT. Such standard shall, to the degree possible, set forth the emissions reductions achievable by implementation of such design, equipment, work practice, or operation and shall provide for compliance by means which achieve equivalent results.

BACT was promulgated within the framework of the PSD requirements in the 1977 amendments of the CAA [Public Law 95-95; Part C, Section 165(a)(4)]. The primary purpose of BACT is to optimize consumption of PSD air quality increments and thereby enlarge the potential for future economic growth without significantly degrading air quality (EPA, 1978; 1980). Guidelines for the evaluation of BACT can be found in EPA's *Guidelines for Determining Best Available Control Technology (BACT)* (EPA, 1978) and in the *PSD Workshop Manual* (EPA, 1980). These guidelines were promulgated by EPA to provide a consistent approach to BACT and to ensure that the impacts of alternative emission control systems are measured by the same set of parameters. In addition, through implementation of these guidelines, BACT in one area may not be identical to BACT in another area. According to EPA (1980), "BACT analyses for the same types of emissions unit and the same pollutants in different locations or situations may determine that different control strategies should be applied to the different sites, depending on site-specific factors. Therefore, BACT analyses must be conducted on a case-by-case basis."

The BACT requirements are intended to ensure that the control systems incorporated in the design of a proposed facility reflect the latest in control technologies used in a particular industry and take into consideration existing and future air quality in the vicinity of the proposed facility. BACT must, as a minimum, demonstrate compliance with new source performance standards (NSPS) for a source (if applicable). An evaluation of the air pollution control techniques and systems, including a cost-benefit analysis of alternative control technologies capable of achieving a higher degree of emission reduction than the proposed control technology, is required. The cost-benefit analysis requires the documentation of the materials, energy, and economic penalties associated with the proposed and alternative control systems, as well as the environmental benefits derived from these systems. A decision on BACT is to be based on sound judgment, balancing environmental benefits with energy, economic, and other impacts (EPA, 1978).

Historically, a "bottom-up" approach consistent with the BACT Guidelines and PSD Workshop Manual has been used. With this approach, an initial control level, which is usually NSPS, is evaluated against successively more stringent controls until a BACT level is selected. However, EPA developed a concern that the bottom-up approach was not providing the level of BACT decisions originally intended. As a result, in December 1987, the EPA Assistant Administrator for Air and Radiation mandated changes in the implementation of the PSD program, including the adoption of a new "top-down" approach to BACT decision making.

The top-down BACT approach essentially starts with the most stringent (or top) technology and emissions limit that have been applied elsewhere to the same or a similar source category. The applicant must next provide a basis for rejecting this technology in favor of the next most stringent technology or propose to use it. Rejection of control alternatives may be based on technical or economic infeasibility. Such decisions are made on the basis of physical differences (e.g., fuel type), locational differences (e.g., availability of water), or significant differences that may exist in the environmental, economic, or energy impacts. The differences between the proposed facility and the facility on which the control technique was applied previously must be justified. EPA has issued a draft guidance

document on the top-down approach entitled *Top-Down Best Available Control Technology Guidance Document* (EPA, 1990).

3.2.3 SOURCE IMPACT ANALYSIS

A source impact analysis must be performed for a proposed major source subject to PSD review for each pollutant for which the increase in emissions exceeds the significant emission rate (Table 3-2). The PSD regulations specifically provide for the use of atmospheric dispersion models in performing impact analyses, estimating baseline and future air quality levels, and determining compliance with AAQS and allowable PSD increments. Designated EPA models normally must be used in performing the impact analysis. Specific applications for other than EPA-approved models require EPA's consultation and prior approval. Guidance for the use and application of dispersion models is presented in the EPA publication *Guideline on Air Quality Models (Revised)*. The source impact analysis for criteria pollutants to address compliance with AAQS and PSD Class II increments may be limited to the new or modified source if the net increase in impacts as a result of the new or modified source is above significance levels, as presented in Table 3-1.

The EPA has proposed significant impact levels (SILs) for Class I areas. The National Park Service (NPS) as the designated agency for oversight in air quality impacts to Class I areas has also recommended significant impact levels for PSD Class I areas. The EPA proposed Class I SILs are as follows:

Pollutant	Averaging Time	Proposed EPA PSD Class I Significant Impact Levels ($\mu\text{g}/\text{m}^3$)
SO_2	3-hour	1
	24-hour	0.2
	Annual	0.1
PM_{10}	24-hour	0.3
	Annual	0.2
NO_2	Annual	0.1

^a $\mu\text{g}/\text{m}^3$ = micrograms per cubic meter.

Although these levels have not been officially promulgated as part of the PSD review process and may not be binding for states in performing PSD review, the proposed levels serve as a guideline in assessing a source's impact in a Class I area. The EPA action to incorporate Class I significant impact levels in the PSD process is part of implementing NSR provisions of the 1990 CAA Amendments. Because the process of developing the regulations will be lengthy, EPA believes that the proposed rules concerning the significant impact levels is appropriate in order to assist states in implementing the PSD permit process.

Various lengths of record for meteorological data can be used for impact analysis. A 5-year period can be used with corresponding evaluation of highest, second-highest short-term concentrations for comparison to AAQS or PSD increments. The term "highest, second-highest" (HSH) refers to the highest of the second-highest concentrations at all receptors (i.e., the highest concentration at each receptor is discarded). The second-highest concentration is significant because short-term AAQS specify that the standard should not be exceeded at any location more than once a year. If fewer than 5 years of meteorological data are used in the modeling analysis, the highest concentration at each receptor normally must be used for comparison to air quality standards.

The term "baseline concentration" evolves from federal and state PSD regulations and refers to a concentration level corresponding to a specified baseline date and certain additional baseline sources. By definition, in the PSD regulations as amended August 7, 1980, baseline concentration means the ambient concentration level that exists in the baseline area at the time of the applicable baseline date. A baseline concentration is determined for each pollutant for which a baseline date is established and includes:

1. The actual emissions representative of facilities in existence on the applicable baseline date; and
2. The allowable emissions of major stationary facilities that commenced construction before January 6, 1975, for SO₂ and PM(TSP) concentrations, or February 8, 1988, for NO₂ concentrations, but that were not in operation by the applicable baseline date.

The following emissions are not included in the baseline concentration and therefore affect PSD increment consumption:

1. Actual emissions from any major stationary facility on which construction commenced after January 6, 1975, for SO₂ and PM(TSP) concentrations, and after February 8, 1988, for NO₂ concentrations; and
2. Actual emission increases and decreases at any stationary facility occurring after the baseline date.

In reference to the baseline concentration, the term "baseline date" actually includes three different dates:

1. The major facility baseline date, which is January 6, 1975, in the cases of SO₂ and PM(TSP), and February 8, 1988, in the case of NO₂.
2. The minor facility baseline date, which is the earliest date after the trigger date on which a major stationary facility or major modification subject to PSD regulations submits a complete PSD application.
3. The trigger date, which is August 7, 1977, for SO₂ and PM(TSP), and February 8, 1988, for NO₂.

The minor source baseline date for SO₂ and PM(TSP) has been set as December 27, 1977, for the entire State of Florida (Rule 62-275.700(1)(a), F.A.C.). The minor source baseline for NO₂ has been set as March 28, 1988 (Rule 62-275.700(3)(a), F.A.C.). It should be noted that references to PM (TSP) are also applicable to PM₁₀.

3.2.4 AIR QUALITY MONITORING REQUIREMENTS

In accordance with requirements of 40 CFR 52.21(m) and Rule 62-212.400(5)(f), F.A.C., any application for a PSD permit must contain an analysis of continuous ambient air quality data in the area affected by the proposed major stationary facility or major modification. For a new major facility, the affected pollutants are those that the facility potentially would emit in significant amounts. For a major modification, the pollutants are those for which the net emissions increase exceeds the significant emission rate (see Table 3-2).

Ambient air monitoring for a period of up to 1 year generally is appropriate to satisfy the PSD monitoring requirements. A minimum of 4 months of data is required. Existing data from the vicinity of the proposed source may be used if the data meet certain quality assurance requirements; otherwise, additional data may need to be gathered. Guidance in designing a PSD monitoring network is provided in EPA's *Ambient Monitoring Guidelines for Prevention of Significant Deterioration* (EPA, 1987a).

The regulations include an exemption that excludes or limits the pollutants for which an air quality analysis must be conducted. This exemption states that Florida DEP may exempt a proposed major stationary facility or major modification from the monitoring requirements with respect to a particular pollutant if the emissions increase of the pollutant from the facility or modification would cause, in any area, air quality impacts less than the *de minimis* levels presented in Table 3-2 (Rule 62-212.400-3, F.A.C.).

3.2.5 SOURCE INFORMATION/GOOD ENGINEERING PRACTICE STACK HEIGHT

Source information must be provided to adequately describe the proposed project. The general type of information required for this project is presented in Section 2.0.

The 1977 CAA Amendments require that the degree of emission limitation required for control of any pollutant not be affected by a stack height that exceeds GEP or any other dispersion technique. On July 8, 1985, EPA promulgated final stack height regulations (EPA, 1985a). Identical regulations have been adopted by Florida DEP (Rule 62-210.550, F.A.C.). GEP stack height is defined as the highest of:

1. 65 meters (m); or
2. A height established by applying the formula:
$$H_g = H + 1.5L$$

where: H_g = GEP stack height,
 H = Height of the structure or nearby structure, and
 L = Lesser dimension (height or projected width) of nearby structure(s); or
3. A height demonstrated by a fluid model or field study.

"Nearby" is defined as a distance up to five times the lesser of the height or width dimensions of a structure or terrain feature, but not greater than 0.8 km. Although GEP stack height regulations require that the stack height used in modeling for determining compliance with AAQS and PSD increments not exceed the GEP stack height, the actual stack height may be greater.

The stack height regulations also allow increased GEP stack height beyond that resulting from the above formula in cases where plume impaction occurs. Plume impaction is defined as concentrations measured or predicted to occur when the plume interacts with elevated terrain. Elevated terrain is defined as terrain that exceeds the height calculated by the GEP stack height formula.

3.2.6 ADDITIONAL IMPACT ANALYSIS

In addition to air quality impact analyses, federal and State of Florida PSD regulations require analyses of the impairment to visibility and the impacts on soils and vegetation that would occur as a result of the proposed source [40 CFR 52.21(o); Rule 62-212.400(5)(e), F.A.C.]. These analyses are to be conducted primarily for PSD Class I areas. Impacts as a result of general commercial, residential, industrial, and other growth associated with the source also must be addressed. These analyses are required for each pollutant emitted in significant amounts (Table 3-2).

3.3 NONATTAINMENT RULES

Based on the current nonattainment provisions (Rule 62-212.500, F.A.C.), all major new facilities and modifications to existing major facilities located in a nonattainment area must undergo nonattainment review. A new major facility is required to undergo this review if the proposed pieces of equipment have the potential to emit 100 TPY or more of the nonattainment pollutant. A major modification at a major facility is required to undergo review if it results in a significant net emission increase of 40 TPY or more of the nonattainment pollutant or if the modification is major (i.e., 100 TPY or more).

For major facilities or major modifications that locate in an attainment or unclassifiable area, the nonattainment review procedures apply if the source or modification is located within the area of influence of a nonattainment area. The area of influence is defined as an area that is outside the boundary of a nonattainment area but within the locus of all points that are 50 km outside the boundary of the nonattainment area. Based on Rule 62-2.500(2)(c)2.a., F.A.C., all VOC sources that are located within an area of influence are exempt from the provisions of NSR for nonattainment areas. Sources that emit other nonattainment pollutants and are located within the area of influence are subject to nonattainment review unless the maximum allowable emissions from the proposed source do not have a significant impact within the nonattainment area.

3.4 EMISSION STANDARDS

3.4.1 NEW SOURCE PERFORMANCE STANDARDS

The NSPS are a set of national emission standards that apply to specific categories of new sources. As stated in the CAA Amendments of 1977, these standards "shall reflect the degree of emission limitation and the percentage reduction achievable through application of the best technological system of continuous emission reduction the Administrator determines has been adequately demonstrated."

The proposed project will be subject to one or more NSPS. The CTs will be subject to 40 CFR Part 60, Subpart GG, and each fuel oil storage tank (2.8 million gallon capacity) will be subject to 40 CFR Part 60, Subpart Kb.

3.4.1.1 Combustion Turbine

The CTs will be subject to emission limitations covered under Subpart GG, which limits NO_x and SO₂ emissions from all stationary combustion turbines with a heat input at peak load equal to 10.7 gigajoules per hour (10 MMBtu/hr), based on the lower heating value of the fuel fired.

NO_x emissions are limited to 75 ppmvd corrected to 15 percent oxygen and heat rate while sulfur dioxide emissions are limited to using a fuel with a sulfur content of 0.8 percent. In

addition to emission limitations, there are requirements for notification, record keeping, reporting, performance testing and monitoring. These are summarized below:

40 CFR 60.7 Notification and Record Keeping

- (a)(1) Notification of the date of construction - 30 days after such date.
- (a)(2) Notification of the date of initial start-up - no more than 60 days or less than 30 days prior to date.
- (a)(3) Notification of actual date of initial start-up - within 15 days after such date.
- (a)(5) Notification of date which demonstrates CEM - not less than 30 days prior to date.

60.7 (b) Maintain records of the start-up, shutdown, and malfunction quarterly.

- (c) Excess emissions reports - by the 30th day following end of quarter. (required even if no excess emissions occur)
- (d) Maintain file of all measurements for two years.

60.8 Performance Tests

- (a) must be performed within 60 days after achieving maximum production rate but no later than 180 days after initial start-up.
- (d) Notification of Performance tests at least 30 days prior to them occurring.

40 CFR Subpart GG

60.334 Monitoring of Operations

- (a) continuous monitoring system required for water-to-fuel ratio to meet NSPS; system must be accurate within ± 5 percent.
- (b) Monitor sulfur and nitrogen content of fuel.
 - Oil - (1): each occasion that fuel is transferred to bulk storage tank.
 - Gas - (2): daily monitoring required

3.4.1.2 Fuel Oil Storage Tank

The applicable NSPS is 40 CFR Part 60, Subpart Kb--Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels for which Construction, Reconstruction, or Modification Commenced after July 23, 1984). The storage tank will contain distillate fuel oil, a volatile organic liquid as defined in Subpart Kb. There are no emission limiting or control requirements under Subpart Kb for the use of distillate fuel oil. The facility, however, must perform record keeping of the type of organic liquid in the tank.

3.4.2 FLORIDA RULES

The Florida DEP regulations for new stationary sources are covered in the F.A.C. The Florida DEP has adopted the EPA NSPS by reference in Rule 62-204.800(7); subsection (b)38 for stationary gas turbines and (b)15 for volatile organic liquid storage vessels. Therefore, the project is required to meet the same emissions, performance testings, monitoring, reporting, and record keeping as those described in Section 3.4.1. DEP has authority for implementing NSPS requirements in Florida.

3.4.3 FLORIDA AIR PERMITTING REQUIREMENTS

The Florida DEP regulations require any new source to obtain an air permit prior to construction. Major new sources must meet the appropriate PSD and nonattainment requirements as discussed previously. Required permits and approvals for air pollution sources include NSR for nonattainment areas, PSD, NSPS, National Emission Standards for Hazardous Air Pollutants (NESHAP), Permit to Construct, and Permit to Operate. The requirements for construction permits and approvals are contained in Rules 62-4.030, 62-4.050, 62-4.052, 62-4.210, and 62-210.300(1), F.A.C. Specific emission standards are set forth in Chapter 62-296, F.A.C.

3.4.4 HAZARDOUS POLLUTANT REVIEW

The Florida DEP has published guidelines (DEP, 1995) to determine whether any emission of a potentially hazardous or toxic pollutant can pose a possible health risk to the public. Maximum concentrations for all regulated pollutants for which an ambient standard does

not exist and all nonregulated hazardous pollutants can be compared to ambient reference concentrations (ARCs) for each applicable pollutant. If the maximum predicted concentrations for any hazardous pollutant is less than the corresponding ARC for each applicable averaging time, that emission is considered not to pose a significant health risk. The ARCs are not environmental standards but, rather, evaluation tools to determine if an apparent threat to the public health may exist. These levels are not used in permitting new sources.

3.4.5 LOCAL AIR REGULATIONS

Hardee County does not have specific air regulations.

3.5 SOURCE APPLICABILITY

3.5.1 AREA CLASSIFICATION

The project site is located in Hardee County, which has been designated by EPA and DEP as an attainment area for all criteria pollutants. Hardee County and surrounding counties are designated as PSD Class II areas for SO₂, PM(TSP), and NO₂. The nearest Class I areas to the site is the Chassahowitzka National Wilderness Area which is about 140 km (88 miles) from the site.

3.5.2 PSD REVIEW

3.5.2.1 Pollutant Applicability

The proposed project is considered to be a major facility because the emissions of several regulated pollutants are estimated to exceed 250 TPY; therefore, PSD review is required for any pollutant for which the emissions are considered major or exceed the PSD significant emission rates. As shown in Table 3-3, potential emissions from the proposed project will be major for PM (TSP), PM₁₀, SO₂, NO_x, CO, VOC, and sulfuric acid mist. Because the proposed project impacts for these pollutants are predicted to be below the significant impact levels, a modeling analysis incorporating the impacts from other sources is not required. (Note: EPA has promulgated changes to the PSD Rules to eliminate hazardous air pollutants (HAPs) from PSD review. The pollutants, vinyl chloride, mercury, asbestos, and beryllium, are no longer evaluated in PSD review.)

As part of the PSD review, a PSD Class I increment analysis is required if the proposed project's impacts are greater than the proposed EPA Class I significant impact levels. The nearest Class I areas to the plant site is about 140 km from the site. A PSD Class I increment-consumption analysis is required.

3.5.2.2 Emission Standards

The applicable NSPS for the CTs is 40 CFR Part 60, Subpart GG. The proposed emissions for the turbines will be well below the specified limits (see Section 4.0). Each fuel oil storage tank will have a maximum storage capacity of 2.8 million gallons of No. 2 fuel oil. Since the storage tank has a capacity greater than 40 cubic meters (m³) [approximately 10,568 gallons], the applicable NSPS is 40 CFR Part 60, Subpart Kb. The storage tank will contain distillate fuel oil, a volatile organic liquid as defined in Subpart Kb, with a true vapor pressure of 0.022 pound per square inch (psi) at 100 F. Because the fuel oil is expected to have a maximum true vapor pressure of less than 3.5 kilopascals (kPa) or 0.51 psi, only the minor monitoring of operating requirements specified in 40 CFR 60 116b(a) and (b) will apply.

3.5.2.3 Ambient Monitoring

Based on the estimated pollutant emissions from the proposed plant (see Table 3-4), a pre-construction ambient monitoring analysis is required for PM₁₀, SO₂, NO₂, CO, and O₃ (based on VOC emissions). If the net increase in impact of other pollutants is less than the applicable *de minimis* monitoring concentration (100 TPY in the case of VOC), then an exemption from the pre-construction ambient monitoring requirement may be obtained [52.21(i)(8)]. In addition, if an acceptable ambient monitoring method for the pollutant has not been established by EPA, monitoring is not required.

If pre-construction monitoring data are required to be submitted, data collected at or near the project site can be submitted, based on existing air quality data or the collection of onsite data.

As shown in Table 3-4, the proposed plant's impacts are predicted to be below the applicable *de minimis* monitoring concentration levels and criteria.

3.5.2.4 GEP Stack Height Impact Analysis

The GEP stack height regulations allow any stack to be at least 65 m [213 feet (ft)] high. The CT stacks for the project will be 60 ft. This stack height does not exceed the GEP stack height. However, as discussed in Section 6.0, Air Quality Modeling Approach, since the stack height is less than GEP, building downwash effects must be considered in the modeling analysis. As a result, the potential for downwash of the CTs' emissions caused by nearby structures are included in the modeling analysis.

3.5.3 NONATTAINMENT REVIEW

The project site is located in Hardee County, which is classified as an attainment area for all criteria pollutants. Therefore, nonattainment requirements are not applicable.

3.5.4 OTHER CLEAN AIR ACT REQUIREMENTS

The 1990 CAA Amendments established a program to reduce potential precursors of acidic deposition. The Acid Rain Program was delineated in Title IV of the CAA Amendments and required EPA to develop the program. EPA's final regulations were promulgated on January 11, 1993, and included permit provisions (40 CFR Part 72), allowance system (Part 73), continuous emission monitoring (Part 75), excess emission procedures (Part 77), and appeal procedures (Part 78).

EPA's Acid Rain Program applies to all existing and new utility units except those serving a generator less than 25 MW, existing simple cycle CTs, and certain non-utility facilities; units which fall under the program are referred to as affected units. The EPA regulations would be applicable to the proposed project for the purposes for obtaining a permit and allowances, as well as emission monitoring. New units are required to obtain permits under the program by submitting a complete application 24 months before the later of January 1, 2000, or the date on which the unit begins serving an electric generator (greater than 25 MW).

The permit would provide SO₂ and NO_x emission limitations and the requirement to hold emission allowances. Emission limitations established in the Acid Rain Program are presumed to be less stringent than BACT or lowest achievable emission rate (LAER) for new units. An allowance is a market-based financial instrument that is equivalent to 1 ton of SO₂ emissions. Allowances can be sold, purchased, or traded. For the proposed project, SO₂ allowances will be obtained from the market.

Continuous emission monitoring (CEM) for SO₂ and NO_x is required for gas-fired and oil-fired affected units. When an SO₂ CEM is selected to monitor SO₂ mass emissions, a flow monitor is also required. Alternately, SO₂ emissions may be determined using procedures established in Appendix D, 40 CFR Part 75 (flow proportional oil sampling or manual daily oil sampling). CO₂ emissions must also be determined either through a CEM (e.g., as a diluent for NO_x monitoring) or calculation. Alternate procedures, test methods, and quality assurance/quality control (QA/QC) procedures for CEM are specified (Part 75 Appendices A through I). The CEM requirements including QA/QC procedures are, in general, more stringent than those specified in the NSPS for Subpart GG. New units are required to meet the requirements by the later of January 1, 1995, or not later than 90 days after the unit commences commercial operation.

Table 3-1. National and State AAQS, Allowable PSD Increments, and Significant Impact Levels

Pollutant	Averaging Time	AAQS ($\mu\text{g}/\text{m}^3$)			PSD Increments ($\mu\text{g}/\text{m}^3$)		Significant Impact Levels ($\mu\text{g}/\text{m}^3$) ^b
		Primary Standard	Secondary Standard	Florida	Class I	Class II	
Particulate Matter ^c (PM ₁₀)	Annual Arithmetic Mean	50	50	50	4	17	1
	24-Hour Maximum	150	150	150	8	30	5
Sulfur Dioxide	Annual Arithmetic Mean	80	NA	60	2	20	1
	24-Hour Maximum	365	NA	260	5	91	5
	3-Hour Maximum	NA	1,300	1,300	25	512	25
Carbon Monoxide	8-Hour Maximum	10,000	10,000	10,000	NA	NA	500
	1-Hour Maximum	40,000	40,000	40,000	NA	NA	2,000
Nitrogen Dioxide	Annual Arithmetic Mean	100	100	100	2.5	25	1
Ozone ^c	8-Hour Maximum ^d	157	157	157	NA	NA	NA
Lead	Calendar Quarter Arithmetic Mean	1.5	1.5	1.5	NA	NA	NA

Note: Particulate matter (PM₁₀) = particulate matter with aerodynamic diameter less than or equal to 10 micrometers.

NA = Not applicable, i.e., no standard exists.

^a Short-term maximum concentrations are not to be exceeded more than once per year.

^b Maximum concentrations are not to be exceeded.

^c On July 18, 1997, EPA promulgated revised AAQS for particulate matter and ozone. For particulate matter, PM_{2.5} standards were introduced with a 24-hour standard g/m^3 (3-year average of 98th percentile) and an annual standard of 15 g/m^3 (3-year average at community monitors). These standards have been stayed by a court case against EPA and implementation of these standards are many years away pending EPA appeal.

^d 0.08 ppm; achieved when 3-year average of 99th percentile is 0.08 ppm or less. These have been stayed by a court case against EPA. EPA is appealing. The 1-hour standard 0.12ppm is still applicable. FDEP has not yet adopted the new standards.

Sources: Federal Register, Vol. 43, No. 118, June 19, 1978.

40 CFR 50; 40 CFR 52.21.

Chapter 62-272, F.A.C.

Table 3-2. PSD Significant Emission Rates and *De Minimis* Monitoring Concentrations

Pollutant	Regulated Under	Significant Emission Rate (TPY)	<i>De Minimis</i> Monitoring Concentration ^a (µg/m ³)
Sulfur Dioxide	NAAQS, NSPS	40	13, 24-hour
Particulate Matter [PM(TSP)]	NSPS	25	10, 24-hour
Particulate Matter (PM ₁₀)	NAAQS	15	10, 24-hour
Nitrogen Dioxide	NAAQS, NSPS	40	14, annual
Carbon Monoxide	NAAQS, NSPS	100	575, 8-hour
Volatile Organic Compounds (Ozone)	NAAQS, NSPS	40	100 TPY ^b
Lead	NAAQS	0.6	0.1, 3-month
Sulfuric Acid Mist	NSPS	7	NM
Total Fluorides	NSPS	3	0.25, 24-hour
Total Reduced Sulfur	NSPS	10	10, 1-hour
Reduced Sulfur Compounds	NSPS	10	10, 1-hour
Hydrogen Sulfide	NSPS	10	0.2, 1-hour
Mercury	NESHAP	0.1	0.25, 24-hour
MWC Organics	NSPS	3.5x10 ⁻⁶	NM
MWC Metals	NSPS	15	NM
MWC Acid Gases	NSPS	40	NM
MSW Landfill Gases	NSPS	50	NM

Note: Ambient monitoring requirements for any pollutant may be exempted if the impact of the increase in emissions is below *de minimis* monitoring concentrations.

NAAQS = National Ambient Air Quality Standards.

NM = No ambient measurement method established; therefore, no *de minimis* concentration has been established.

NSPS = New Source Performance Standards.

NESHAP = National Emission Standards for Hazardous Air Pollutants.

g/m³ = micrograms per cubic meter.

MWC = Municipal waste combustor

MSW = Municipal solid waste

^a Short-term concentrations are not to be exceeded.

^b No *de minimis* concentration; an increase in VOC emissions of 100 TPY or more will require monitoring analysis for ozone.

^c Any emission rate of these pollutants.

Sources: 40 CFR 52.21.

Rule 62-212.400

Table 3-3. Maximum Emissions Due to the Proposed IPS Vandolah Power Project Compared to the PSD Significant Emission Rates

Pollutant	Pollutant Emissions (TPY)		PSD Review
	Potential Emissions from Proposed Facility ^a	Significant Emission Rate	
Sulfur Dioxide	221.1	40	Yes
Particulate Matter [PM(TSP)]	81.8	25	Yes
Particulate Matter (PM ₁₀)	81.8	15	Yes
Nitrogen Dioxide	1,007.8	40	Yes
Carbon Monoxide	345.9	100	Yes
Volatile Organic Compounds	45.9	40	Yes
Lead	0.04	0.6	No
Sulfuric Acid Mist	33.9	7	Yes
Total Fluorides	0.12	3	No
Total Reduced Sulfur	NEG	10	No
Reduced Sulfur Compounds	NEG	10	No
Hydrogen Sulfide	NEG	10	No
Mercury	0.002	0.1	No
MWC Organics (as 2,3,7,8-TCDD)	1.3X10 ⁻⁶	3.5x10 ⁻⁶	No
MWC Metals (as Be, Cd)	0.014	15	No
MWC Acid Gaser (as HCl)	0.8	40	No

Note: NEG = Negligible.

^a Based on emissions from operating at baseload at 59°F; firing natural gas and distillate fuel oil for 1,390 and 2,000 hours per year per turbine for a total of four CTs, respectively (Refer to Table 2-7).

Table 3-4. Predicted Net Increase in Impacts Due to the Proposed IPS Vandolah Power Project Compared to PSD *De Minimis* Monitoring Concentrations

Pollutant	Concentration ($\mu\text{g}/\text{m}^3$)	
	Predicted Increase in Impacts ^a	<i>De Minimis</i> Monitoring Concentration
Sulfur Dioxide	1.0	13, 24-hour
Particulate Matter (PM_{10})	0.2	10, 24-hour
Nitrogen Dioxide	0.3	14, annual
Carbon Monoxide	49	575, 8-hour
Volatile Organic Compounds	45.9 TPY	100 TPY

Note: NA = not applicable.

NM = no ambient measurement method.

TPY = tons per year.

^a See Section 6.0 for air dispersion modeling results.

4.0 CONTROL TECHNOLOGY REVIEW

4.1 APPLICABILITY

The PSD regulations require new major stationary sources to undergo a control technology review for each pollutant that may potentially be emitted above significant amounts. The control technology review requirements of the PSD regulations are applicable to emissions of NO_x, SO₂, CO, VOC, and PM/PM₁₀ (see Section 3.0). The maximum potential annual emissions of these pollutants from the proposed GE 7FA CTs are summarized below (see Table 2-7):

Pollutant Emissions (TPY)	
Pollutant	4 GE 7FA CTs
NO _x	1,007.8
SO ₂	221.1
CO	345.9
VOC	45.9
PM/PM ₁₀	81.8

^a Maximum emissions based on firing natural gas for 2,390 hours and distillate fuel oil for 1,000 hours at baseload conditions and 59°F.

This section presents the applicable NSPS and the proposed BACT for these pollutants. The approach to the BACT analysis is based on the regulatory definitions of BACT, as well as EPA's current policy guidelines requiring a top-down approach. A BACT determination requires an analysis of the economic, environmental, and energy impacts of the proposed and alternative control technologies [see 40 CFR 52.21(b)(12); and Rule 62-212.200(40), and Rule 62-214.410, F.A.C.]. The analysis must, by definition, be specific to the project (i.e., case-by-case).

4.2 NEW SOURCE PERFORMANCE STANDARDS

The applicable NSPS for CTs are codified in 40 CFR 60, Subpart GG and summarized in Appendix B. The applicable NSPS emission limit for NO_x is 75 parts per million by volume

dry (ppmvd) corrected for heat rate and 15 percent oxygen. For the CTs being considered for the project, the NSPS emission limit NO_x with the NSPS heat rate correction is 109.4 parts per million (ppm) on gas and 103.1 ppm on oil (corrected to 15 percent oxygen at a fuel-bound nitrogen content of 0.015 percent. The proposed NO_x emission limits for the project will be much lower than the NSPS.

4.3 BEST AVAILABLE CONTROL TECHNOLOGY

4.3.1 PROPOSED BACT

In recent permitting actions, FDEP has established BACT for heavy-duty industrial gas turbines. These decisions have included the use of advanced dry low- NO_x combustors for limiting NO_x and CO emissions and clean fuels (natural gas and distillate oil) for control of other emissions, including SO_2 . The BACT proposed for the CTs is consistent with these FDEP permits. The proposed project will have two modes of operation (see Section 2.3) for which a BACT analysis has been performed. The results of the analysis have concluded the following controls as BACT for the project.

1. Natural Gas Fired. The CTs will utilize state-of-the-art dry low- NO_x combustion technology which will achieve gas turbine exhaust NO_x levels of no greater than 9ppmvd corrected to 15 percent O_2 . CO emissions will be limited to 12 ppmvd at baseload.
2. Fuel Oil Fired. The CT will utilize water injection to achieve gas turbine exhaust NO_x levels of no greater than 42 ppmvd corrected to 15 percent O_2 . CO emissions will be limited to 20 ppmvd at baseload.

4.3.2 NITROGEN OXIDES

4.3.2.1 Introduction

The BACT analysis was performed for the following alternatives:

1. Advanced dry low- NO_x combustors at an emission rate of 9 ppmvd corrected to 15 percent O_2 when firing gas and 42 ppmvd (corrected) when firing oil.
2. Selective catalytic reduction (SCR) and advanced dry low- NO_x combustors at an emission rate of approximately 3.6 ppmvd corrected to 15 percent O_2 when firing natural gas and 16.8 ppmvd when firing oil.

Appendix B presents a discussion of NO_x control technologies and their feasibility for the project.

Dry low-NO_x combustor technology has recently been offered and installed by manufacturers to reduce NO_x emissions by inhibiting thermal NO_x formation through premixing fuel and air prior to combustion and providing staged combustion to reduce flame temperatures. NO_x emissions from 25 ppmvd (corrected to 15-percent O₂) and less has been offered by manufacturers for advanced combustion turbines. Advanced in this context is the larger (over 150 MW) and more efficient (higher initial firing temperatures and lower heat rate) combustion turbines. This technology is truly pollution prevention since NO_x emissions are inhibited from forming.

SCR is a post-combustion process where NO_x in the gas stream is reacted with ammonia in the presence of a catalyst to form nitrogen and water. The reaction occurs typically between 600°F and 750°F, which has limited SCR application to combined cycle units where such temperatures occur in the HRSG. Exhausts from simple cycle operation up to 1,200°F, thus limiting SCR application for this mode of operation. With the higher cost ceramic catalyst, temperatures up to 1,050°F are possible. Such SCR systems are referred to as "hot" SCR. To accommodate "hot" SCR in the "F" Class gas turbine, some gas cooling would be required to maintain temperatures below 1,050°F. In-duct cooling using about 110,000 acfm of ambient air would maintain temperatures at below 1,050°F with turbine flow of about 2,600,000 acfm and up to 1,200°F. This could be accomplished with an electric powered fan rated at about 200 kW. While such modifications are theoretically possible, such gas cooling and its effectiveness has not been demonstrated on a "F" Class simple cycle gas turbine. SCR has been primarily installed and operated on combined cycle facilities using catalysts with temperature ranges from 600-750°F and generally achieving 9 ppmvd (corrected to 15-percent O₂) or less while burning only natural gas.

Applications of SCR with oil firing are limited. Where oil firing has been attempted, catalyst poisoning and ammonium salt formation has occurred. Ammonium salts (ammonium

sulfate and ammonium bisulfate) are formed by the reaction of sulfur oxides in the gas stream and ammonia. These salts are highly acidic, and special precautions in materials and ammonia injection rates must be implemented to minimize their formation. Ammonia injected in the SCR system that does not react with NO_x is emitted directly and referred to as ammonia slip. In general, SCR manufacturers guarantee ammonia slip to be no more than 10 ppmvd; however, permitted limits in some applications have exceeded 25 ppmvd. While SCR is technically feasible for the project, SCR has not been applied to a simple cycle advanced combustion turbine of the size proposed for this project or to the amount of oil firing that may occur.

The recent permitting trend for advanced combustion turbines, even with combined cycle configuration, is the use of dry low- NO_x combustors. Indeed, most of the recent Florida projects have been permitted with this technology, including five projects in Florida (Florida Power & Light Martin Units 3 and 4; Central Florida Cogeneration Project; Hardee Unit 3 Project, and City of Tallahassee Project), and FPL Fort Myers Repowering Project.

As discussed in Section 2.1, the proposed CTs will be fired primarily with natural gas. Distillate oil will be used as backup fuel not to exceed 1,000 hours per year. Table 4-1 presents a summary of emissions with dry low- NO_x combustors and with dry low- NO_x combustors and SCR assuming 39 percent operating capacity at an ambient temperature of 59°F. The NO_x removed using SCR would be 151 TPY when firing oil and natural gas. The NO_x removed when firing oil is based on 1,000 hours per year. The NO_x removed when firing natural gas is based on 2,390 hours of operation.

4.3.2.2 Proposed BACT and Rationale

The proposed BACT for the project is advanced dry low- NO_x combustion technology. The proposed NO_x emissions level using this technology is 9 ppmvd (corrected to 15 percent oxygen) when firing natural gas under baseload conditions. NO_x from oil firing will be controlled using water injection (42 ppmvd corrected to 15 percent oxygen). This combination of control technologies is proposed for the following reasons:

1. SCR was rejected based on technical, economic, environmental, and energy grounds. Table 4-2 summarizes these considerations which favor the dry low-NO_x pollution prevention technology.
2. The estimated incremental cost of SCR is approximately 14,900 per ton of NO_x removed and is similar to cost for other projects that have rejected SCER as being unreasonable. This is even more apparent if additional pollutant emissions due to SCR are considered.
3. Additional environmental impacts would result from SCR operation, including emissions of ammonia; from secondary emissions (to replace the lost generation); and from the generation of hazardous waste (i.e., spent catalyst replacement). While NO_x emissions would be reduced by about 151 TPY per unit with SCR, the net emissions reduction would not be as great. There are three additional factors that must be considered:
 - a. Ammonia slip would occur, and it may be as high as 40.4 TPY per unit.
 - b. Additional particulate matter may be formed through the reaction of ammonia and sulfur oxides forming ammonium salts. As much as 17.1 TPY per unit additional particulate matter may be formed.
 - c. SCR will require energy for system operation and reduce the efficiency of the combustion turbine. This lost energy would have to be replaced since the proposed project would be an efficient peaking power plant while operating. Any peaking power plants replacing this lost energy would be lower on the dispatch list and inevitably more polluting. Conservatively, this lost energy would result in the emissions of an additional 4.7 TPY of criteria pollutants. Additional emissions of carbon dioxide would also result.
 - d. The "net" cost effectiveness could be as high as \$25,300 per ton of pollutant removed.
4. The energy impacts of SCR will reduce potential electrical power generation by more than 3.9 million kilowatt hours (kWh) per year. This amount of energy is sufficient to provide the monthly electrical needs of 1,200 residential customers.
5. The proposed BACT (i.e., dry low-NO_x combustion) provides the most cost effective control alternative, is pollution preventing, and results in low

environmental impacts (less than the significant impact levels). Dry low-NO_x combustion at the proposed emissions levels has been adopted previously in BACT determinations. Indeed, compared to conventional CTs, the proposed BACT will result in 10 to 15 percent less NO_x emission from the same amount of generation.

The analyses of economic, environmental, and energy impacts follow.

4.3.2.3 Impact Analysis

Economic--The total capital costs of SCR for the proposed plant are \$5,263,200 per CT. The total annualized cost of applying SCR with dry low-NO_x combustion is \$2,250,700. Appendix B contains the detailed cost estimates for the capital and annualized costs. The incremental cost effectiveness of adding SCR to the dry low-NO_x combustors and water injection (for oil firing) is estimated at \$14,900 per ton of NO_x removed.

Environmental--The maximum predicted NO_x impacts using the dry low-NO_x technology are all considerably below the NO₂ PSD Class II increment of 25 µg/m³, annual average, and the AAQS of 100 µg/m³, annual average. Indeed, the maximum annual impact for the project is 0.3 µg/m³, which is about 30 percent of the significant impact level. While additional controls beyond dry low-NO_x combustors (i.e., SCR and SCR with water injection) would reduce emissions, the effect will not be significant and much less than 1 percent of the PSD increment and the AAQS for the project.

The use of dry low-NO_x combustor technology is truly "pollution prevention". In contrast, use of SCR on the proposed project will cause emissions of ammonia and ammonium salts, such as ammonium sulfate and bisulfate. Ammonia emissions associated with SCR are expected to be up to 10 ppm based on reported experience; previous permit conditions have specified this level. Indeed, ammonia emissions could be as high as 40.4 TPY/ per unit for the project. Potential emissions of ammonium sulfate and bisulfate will increase emissions of PM₁₀; up to 17.1 TPY/per unit could be emitted.

The electrical energy required to run the SCR system and the back pressure from the turbine will reduce the available power from the project. This power, which would otherwise be available to the electrical system, will have to be replaced by other less efficient units. The replacement power will cause air pollutant emissions that would not have occurred without SCR. These "secondary" emissions, coupled with potential emissions of ammonia and ammonium salts, are presented in Table 4-3. This table shows the emissions balance for the project with and without SCR. As shown, the net reduction in emissions with SCR when all criteria pollutants are considered will be 89 TPY. In addition to criteria pollutants, additional secondary emissions of carbon dioxide would be emitted and were included in Table 4-3. As noted from this table, the emissions including CO₂ would be greater with SCR than that proposed using dry low-NO_x combustion technology.

The replacement of the SCR catalyst will create additional economic and environmental impacts since certain catalysts contain materials that are listed as hazardous chemical wastes under Resource Conservation and Recovery Act (RCRA) regulations (40 CFR 261). In addition, SCR will require the construction and maintenance of storage vessels of anhydrous or aqueous ammonia for use in the reaction. Ammonia has potential health effects, and the construction of ammonia storage facilities triggers the application of at least three major standards: Clean Air Act (section 112), Occupational Safety and Health Administration (OSHA) 29 CFR 1910.1000, and OSHA 29 CFR 1910.119.

Energy--Significant energy penalties occur with SCR. With SCR, the output of the CT may be reduced by about 0.50 percent over that of advanced low-NO_x combustors. This penalty is the result of the SCR pressure drop, which would be about 2.5 inches of water and would amount to about 2,967,290 kWh per year in potential lost generation. The energy required by the SCR equipment would be about 949,200 kWh per yr. Taken together, the total lost generation and energy requirements of SCR of 3,916,490 kWh per year could supply the monthly electrical needs of about 326 residential customers. To replace this lost energy, an additional 41×10^{10} British thermal units per year (Btu/yr) or about 41 million cubic feet per year (ft³/yr) of natural gas would be required.

Technology Comparison--The proposed project will use an advanced heavy-duty industrial gas turbine with advanced dry low-NO_x combustors. This type of machine advances the state-of-the-art for CTs by being more efficient and less polluting than previous CTs. Integral to the machine's design is dry low-NO_x combustors that prevent the formation of air pollutants within the combustion process, thereby eliminating the need for add-on controls that can have detrimental effects on the environment. An analogy of this technology is a more efficient automotive engine that gives better mileage and reduces pollutant formation without the need of a catalytic converter.

An advanced gas turbine is unique from an engineering perspective in two ways. First, the advanced machine is larger and has higher initial firing (i.e., combustion) temperatures than conventional turbines. This results in a larger, more thermally efficient machine. For example, the electrical generating capability of the proposed GE Frame 7 FA advanced machine is about 170 MW compared to the 70 MW to 120 MW conventional machines. The higher initial firing temperature (i.e., 2,600°F) results in about 20 percent more electrical energy produced for the same amount of fossil fuel used in conventional machines. This has the added advantage of producing lower air pollutant emissions (e.g., NO_x, PM, and CO) for each MW generated. While the increased firing temperature increases the thermal NO_x generated, this NO_x increase is controlled through combustor design.

The second unique attribute of the advanced machine is the use of dry low-NO_x combustors that will reduce NO_x emissions to 9 ppmvd when firing natural gas. Thermal NO_x formation is inhibited by using staged combustion techniques where the natural gas and combustion air are premixed prior to ignition. This level of control will result in NO_x emissions of about 0.04 lb/10⁶ Btu, which is less than half of the emissions generated from conventional fossil fuel-fired steam generators.

Since the purpose of the project is to produce electrical energy, and CT technology is rapidly advancing, it is appropriate to compare the proposed emissions on an equivalent generation basis to that of a conventional CT. The heat rate of the GE 7FA machines will be about 9,360 Btu/kWh (LHV, 59°F, natural gas). In contrast, the heat rate for a new conventional CT

is about 11,000 Btu/kWh. Therefore, the amount of total NO_x from the advanced CT will be more than 10-percent lower than a conventional turbine for the same amount of generation.

Also, the amount of NO_x control achieved by the dry low-NO_x combustor on an advanced CT is considerably higher than that achieved by a conventional CT. Because of the higher firing initial temperatures, the advanced CT results in greater NO_x emission formation. Since the advanced machine has higher firing temperatures, the NO_x emissions without the use of dry low-NO_x combustion technology are much higher than a conventional CT (greater than 180 ppmvd vs. 150 ppmvd). This results in an overall greater NO_x reduction on the advanced CT.

4.3.3 CARBON MONOXIDE

4.3.3.1 Introduction

Emissions of CO are dependent upon the combustion design, which is a result of the manufacturer's operating specifications, including the air-to-fuel ratio, staging of combustion, and the amount of water injected (i.e., for oil firing). The CTs proposed for the project have designs to optimize combustion efficiency and minimize CO as well as NO_x emissions.

For the project, the following alternatives were evaluated as BACT:

1. Combustion controls at 12 ppmvd when firing natural gas (at baseload) and 20 ppmvd when firing oil (at baseload); and
2. Oxidation catalyst at 80% removal; maximum annual CO emissions are 17 TPY per unit.

4.3.3.2 Proposed BACT and Rationale

Combustion design is proposed as BACT, as there are adverse technical and economic consequences of using catalytic oxidation on CTs. The proposed BACT emission rates for CO will not exceed 12 ppmvd when firing natural gas and 20 ppmvd when firing distillate oil at baseload conditions. Catalytic oxidation is considered unreasonable for the following reasons:

1. Catalytic oxidation will not produce measurable reduction in the air quality impacts;
2. The economic impacts are significant (i.e., the capital cost is about \$1.7 million per unit, with an analyzed cost of \$466,000 per year per unit); and
3. Recent projects in Florida have been authorized with BACT emission limits of 25 ppmvd on gas and 90 ppmvd on oil.

Combustion design is proposed as BACT as a result of the technical and economic consequences of using catalytic oxidation on CTs. Catalytic oxidation is considered unreasonable since it will not produce a measurable reduction in the air quality impacts. Indeed, recent BACT decisions for similar advanced CTs have set limits in the 30 ppmvd range and higher. Even the Northeast States for Coordinated Air Use Management (NESCAUM) has recognized a BACT level of 50 ppmvd for CO emissions. The cost of an oxidation catalyst would be significant and not be cost effective given the maximum proposed emission limits.

4.3.3.3 Impact Analysis

Economic--The estimated annualized cost of a CO oxidation catalyst is \$466,000 per unit, resulting in a cost effectiveness of greater than \$9,000 per ton of CO removed. The cost effectiveness is based on 2,390 hours per year on natural gas and 1,000 hours per year of operation on oil. No costs are associated with combustion techniques since they are inherent in the design.

Environmental--The air quality impacts of both oxidation catalyst control and combustion design control techniques are below the significant impact levels for CO. Therefore, no significant environmental benefit would be realized by the installation of a CO catalyst. Moreover, the air quality impacts at the proposed CT emission rate are predicted to be much less than the PSD significant impact levels. The maximum CO impacts are less than 0.1 percent of the applicable ambient air quality standards. There would also be no secondary benefits, such as reductions in acidic deposition, to reducing CO.

Energy--An energy penalty would result from the pressure drop across the catalyst bed. A pressure drop of about 2 inches water gauge would be expected. At a catalyst back pressure of about 2 inches, an energy penalty of about 1,186,900 kWh/yr would result at 100 percent load. This energy penalty is sufficient to supply the electrical needs of about 99 residential customers for a year. To replace this lost energy, about 1.2×10^{10} Btu/yr or about 12 million ft³/yr of natural gas would be required.

4.3.4 VOLATILE ORGANIC COMPOUNDS

VOCs will be emitted by the CT as a result of incomplete combustion. The proposed BACT for VOC emissions will be the use of combustion technology and the use of clean fuels so that emissions will not exceed 1.4 ppmvd when firing natural gas and 7.0 ppmvw when firing distillate oil. These emission levels are similar to the BACT emission levels established for other similar sources. Combustion controls and the use of clean fuels have been overwhelmingly approved as BACT for CTs. The environmental effect of further reducing emissions would not be significant.

4.3.5 PM/PM₁₀/ SO₂ AND OTHER REGULATED AND NONREGULATED POLLUTANT EMISSIONS

The PM/PM₁₀ emissions from the CTs are a result of incomplete combustion and trace elements in the fuel. The design of the CT ensures that particulate emissions will be minimized by combustion controls and the use of clean fuels. A review of EPA's BACT/LAER Clearinghouse Documents did not reveal any post-combustion particulate control technologies being used on gas- or oil-fired CTs.

The maximum particulate emissions from the CT will be lower in concentration than that normally specified for fabric filter designs {i.e., the grain loading associated with the maximum particulate emissions [about 10 pounds per hour (lb/hr) when firing natural gas]} is less than 0.01 grain per standard cubic foot (gr/scf), which is a typical design specification for a baghouse. This further demonstrates that no further particulate controls are necessary for the proposed project.

There are no technically feasible methods for controlling the emissions of these pollutants from CTs, other than the inherent quality of the fuel. Clean fuels, natural gas and distillate oil represent BACT for these pollutants. The use of natural gas and very low sulfur (0.05%) fuel oil will limit emissions of SO₂.

For the nonregulated pollutants, none of the control technologies evaluated for other pollutants (i.e., SCR) would reduce such emissions; thus, natural gas and distillate oil represent BACT because of their inherently low contaminant content.

Table 4-1. NO_x Emission Estimates (TPY) of BACT Alternative Technologies (per Unit)

Alternative BACT Control Technologies	Operating Mode ^a		Total
	Oil	Gas	
<u>NO_x Emission (TPY)</u>			
Dry Low-NO _x (DLN) only	175.4	76.6	252.0
DLN with SCR ^b	70.2	30.6	100.8
Reduction	(105.2)	(46.0)	(151.2)
<u>Basis of Emissions (ppmvd)</u>			
DLN only	42	9	
DLN with SCR	16.8	3.6	
Hours of Operation	1,000	2,390	3,390

Note: DLN = Dry low-NO_x.

SCR = selective catalytic reduction.

TPY = tons per year.

^a Emission rates were based on a "F" class combustion turbine operating at 100-percent capacity and firing natural gas for 2,390 hours and distillate fuel oil for 1,000 hours. Emission data are based on an ambient temperature of 50°F at maximum emission rates.

^b Based on primary emissions with SCR; no account is made for additional emissions (secondary) due to lost energy from heat rate penalty and electrical usage for SCR operation (see Table 4-3).

Table 4-2. Comparison of Alternative BACT Control Technologies for NO_x (per Unit)

	Alternative BACT Control Technologies	
	DLN Only	SCR
Technical Feasibility	Feasible	Feasible for gas
Economic Impact ^a		
Capital Costs	included	\$5,263,200
Annualized Costs	included	\$2,250,700
Cost Effectiveness		
NO _x Removed (per ton of NO _x)	NA	\$14,886
NO _x Removed (per ton of total pollutants)	NA	25,267
Environmental Impact ^b		
Total NO _x (TPY)	252	101
NO _x Reduction (TPY)	NA	(151.2)
Ammonia Emissions (TPY)	0	40.4
PM Emissions (TPY)	0	17.1
Secondary Emissions (TPY)	0	4.7
Net Emission Reduction (TPY)	NA	(89.1)
Energy Impacts ^c		
Energy Use (kWh/yr)	0	3,916,490
Energy Use (mmBtu/yr)		
at 10,000 Btu/kWh	0	40,696
Energy Use (mmcf/yr)		
at 1,000 Btu/cf for natural gas	0	41
Energy Use (residential customers)	0	326

^a See Appendix B for detailed development of capital costs (including recurring costs) and annualized costs.

^b See emission data presented in Table 4-3.

^c Energy impacts are estimated due to the lost energy from heat rate penalty and electrical usage for the SCR operation at 3,390 hours per year. Lost energy is based on 0.5 percent of 175.06 MW. SCR electrical usage is based on 0.080 MWh per SCR system and 0.20 MWh for cooling fan.

Table 4-3. Maximum Potential Incremental Emissions (TPY) with Selective Catalytic Reduction

Pollutants	Incremental Emissions (tons/year) of SCR		Total
	Primary	Secondary	
Particulate	17.10	0.15	17.25
Sulfur Dioxide		0.06	0.06
Nitrogen Oxides	-151.20	2.71	-148.49
Carbon Monoxide		1.63	1.63
Volatile Organic Compounds		0.11	0.11
Ammonia	40.37		
Total:	-93.73	4.65	-89.08
Carbon Dioxide (additional from gas firing)		2,577.43	2,577.43

Basis:

Lost Energy (mmBtu/year) 40,696

Secondary Emissions (lb/mmBtu): Assumes natural gas firing in NO_x controlled steam unit.

Particulate 0.0072

Sulfur Dioxide 0.0027

Nitrogen Oxides w/LNB 0.1333

Carbon Monoxide 0.0800

Volatile Organic Compounds 0.0052

Reference: Table 1.4-1 and 1.4-2, AP-42, Version 2/98

5.0 AMBIENT MONITORING ANALYSIS

The CAA requires that an air quality analysis be conducted for each criteria and noncriteria pollutant subject to regulation under the act before a major stationary source is constructed. Criteria pollutants are those pollutants for which AAQS have been established. Noncriteria pollutants are those pollutants that may be regulated by emission standards, but no AAQS have been established. This analysis may be performed by the use of modeling and/or by monitoring the air quality.

A major source may waive the ambient monitoring analysis requirement if it can be demonstrated that the proposed source's maximum air quality impacts will not exceed the PSD *de minimis* concentration levels. The maximum impacts of the proposed source are compared with the PSD *de minimis* concentrations in Table 3-4. As can be seen from Table 3-4, the proposed plant's maximum air quality impacts will be well below the *de minimis* concentrations for all applicable pollutants. For VOCs, the potential emission from the project are less than the *de minimis* criteria of 100 TPY; therefore, monitoring for ozone is not required.

6.0 AIR QUALITY IMPACT ANALYSIS

6.1 SIGNIFICANT IMPACT ANALYSIS APPROACH

The general modeling approach in this case followed EPA and Florida DEP modeling guidelines for determining compliance with AAQS and PSD increments. For all applicable pollutants that have emission increases that will exceed the PSD significant emission rate due to a proposed project, a significant impact analysis is performed to determine whether the project alone will result in predicted impacts that will exceed the EPA significant impact levels at any off-plant property areas in the vicinity of the plant.

If the project's impacts are above the significant impact levels, then a more detailed air modeling analysis that includes background sources is performed. Current Florida DEP policies stipulate that the highest annual average and highest short-term (i.e., 24 hours or less) concentrations are to be compared to the applicable significant impact levels. Based on the screening modeling analysis results, additional modeling refinements with a denser receptor grid are performed, as necessary, to obtain the maximum concentration. Modeling refinements are performed with a receptor grid spacing of 100 meters (m) or less.

For this project, the significant impacts levels were estimated in the vicinity of the plant following Florida DEP policies.

Generally, if a new project also is within 150 km of a PSD Class I area, then a significant impact analysis is also performed for the PSD Class I area. Currently, the National Park Service (NPS) has recommended significant impact levels for PSD Class I areas. The recommended levels have not been promulgated as rules. EPA also has proposed PSD Class I significant impact levels that have not been finalized as of this report.

Because the proposed project site is approximately 139 km from the Chassahowitzka National Wildlife Refuge (CNWR) PSD Class I area, a significant impact modeling analysis has been performed.

6.2 PRECONSTRUCTION MONITORING ANALYSIS APPROACH

The general modeling approach in this case followed EPA and Florida DEP modeling guidelines for evaluating a project's impacts relative to the *de minimis* monitoring levels to determine the need to submit continuous monitoring data prior to construction. For all applicable pollutants that have emission increases that will exceed the PSD significant emission rate due to a proposed project, a *de minimis* impact analysis is performed to determine whether the project alone will result in predicted impacts that will exceed the EPA *de minimis* levels at any off-plant property areas in the vicinity of the plant. Current Florida DEP policies stipulate that the highest annual average and highest short-term concentrations are to be compared to the applicable *de minimis* monitoring levels.

A proposed major stationary facility or major modification may be exempt from the monitoring requirements with respect to a particular pollutant if the emissions increase of the pollutant from the facility or modification would cause, in any area, air quality impacts less than the *de minimis* levels.

For this project, the project's impacts were estimated in the vicinity of the plant for comparison to *de minimis* levels following Florida DEP policies. As presented in Section 5.0, since the estimated project's VOC emissions are lower than the *de minimis* VOC emission level, the project is exempt from preconstruction ambient monitoring requirements.

6.3 AIR MODELING ANALYSIS APPROACH

6.3.1 GENERAL PROCEDURES

As stated in the previous sections, for each pollutant which is emitted above the significant emission rate, air modeling analyses are required to determine if the project's impacts are predicted to be greater than the significant impact levels and *de minimis* monitoring levels. These analyses consider the project's impacts alone. Air quality impacts are predicted using 5 years of meteorological data and selecting the highest annual and the highest short-term concentrations for comparison are compared to the significant impact levels and *de minimis* levels.

If the project's impacts are greater than the significant impact levels, the air modeling analyses must consider other nearby sources and background concentrations, and predict concentration for comparison to ambient standards. In general, when 5 years of meteorological data are used in the analysis, the highest annual and the highest, second-highest (HSH) short-term concentrations are compared to the applicable AAQS and allowable PSD increments. The HSH concentration is calculated for a receptor field by:

1. Eliminating the highest concentration predicted at each receptor,
2. Identifying the second-highest concentration at each receptor, and
3. Selecting the highest concentration among these second-highest concentrations.

This approach is consistent with air quality standards and allowable PSD increments, which permit a short-term average concentration to be exceeded once per year at each receptor.

To develop the maximum short-term concentrations for the proposed project, the modeling approach was divided into screening and refined phases to reduce the computation time required to perform the modeling analysis. For this study, the only difference between the two modeling phases is the density of the receptor grid spacing employed when predicting concentrations. Concentrations are predicted for the screening phase using a coarse receptor grid and a 5-year meteorological data record.

Refinements of the maximum predicted concentrations are typically performed for the receptors of the screening receptor grid at which the highest and/or HSH concentrations occurred over the 5-year period. Generally, if the maximum concentration from other years in the screening analysis are within 10 percent of the overall maximum concentration, then those other concentrations are refined as well. Typically, if the highest and HSH concentrations are in different locations, concentrations in both areas are refined.

Modeling refinements are performed for short-term averaging times by using a denser receptor grid, centered on the screening receptor at which the maximum concentration was predicted. The angular spacing between radials is 2 degrees and the radial distance interval between receptors is 100 m. Annual modeling refinements employ an angular spacing between radials of 2 degrees and a distance interval from 100 to 300 m, depending on the

concentration gradient in the vicinity of the screening receptor to be refined. If the maximum screening concentration is located on the plant property boundary, additional plant boundary receptors are input, spaced at a 2-degree angular interval and centered on the screening receptor. The domain of the refinement grid will extend to all adjacent screening receptors. The air dispersion model is then executed with the refined grid for the entire year of meteorology during which the screening concentration occurred. This approach is used to ensure that a valid highest concentration is obtained. A more detailed description of the model, along with the emission inventory, meteorological data, and screening receptor grids are presented in the following sections.

6.3.2 MODEL SELECTION

The Industrial Source Complex Short-term (ISCST3, Version 98356) dispersion model (EPA, 1997) was used to evaluate the pollutant impacts due to the proposed CTs. This model is maintained by the EPA on its Internet website, Support Center for Regulatory Air Models (SCRAM), within the Technical Transfer Network (TTN). A listing of ISCST3 model features is presented in Table 6-1. The ISCST3 model is designed to calculate hourly concentrations based on hourly meteorological data (i.e., wind direction, wind speed, atmospheric stability, ambient temperature, and mixing heights). The ISCST3 model is applicable to sources located in either flat or rolling terrain where terrain heights do not exceed stack heights. These areas are referred to as simple terrain. The model can also be applied in areas where the terrain exceeds the stack heights. These areas are referred to as complex terrain.

In this analysis, the EPA regulatory default options were used to predict all maximum impacts. The ISCST3 model can run in the rural or urban land use mode which affects stability dispersion coefficients, wind speed profiles, and mixing heights. Land use can be characterized based on a scheme recommended by EPA (Auer, 1978). If more than 50 percent land use within a 3-km radius around a project is classified as industrial or commercial, or high-density residential, then the urban option should be selected. Otherwise, the rural option is appropriate. Based on the land-use within a 3-km radius of the proposed plant site (see Figure 2-1), the rural dispersion coefficients were used in the modeling analysis.

The ISCST3 model was used to provide maximum concentrations for the annual and 24-, 8-, 3-, and 1-hour averaging times. A generic emission rate of 10 grams per second (g/s) was used as emissions for the proposed source. Maximum pollutant-specific air impacts were determined by multiplying the maximum pollutant-specific emission rate in pounds per hour (lb/hr) to the maximum predicted generic impact divided by 79.365 lb/hr (10 g/s).

6.3.3 METEOROLOGICAL DATA

Meteorological data used in the ISCST3 model to determine air quality impacts consisted of a concurrent 5-year period of hourly surface weather observations and twice-daily upper air soundings from the National Weather Service (NWS) stations at the Tampa International Airport in Tampa, Florida, and at Ruskin, Florida, respectively. The 5-year period of meteorological data was from 1987 through 1991. The NWS station at Tampa is located approximately 74 km (46 miles) to the north of the proposed plant site while the NWS station at Ruskin is located approximately 56 km (35 miles) west-northwest of the proposed plant site. The surface meteorological data from Tampa are assumed to be representative of the project site because both the project site and the weather station are located in similar topographical areas and are situated in central Florida to experience similar weather conditions, such as frontal passages.

6.3.4 EMISSION INVENTORY

A summary of the criteria pollutant emission rates, physical stack and stack operating parameters for the proposed CTs used in the air modeling analysis is presented in Tables 2-1 through 2-6. The emission and stack operating parameters presented for 32°F and 95°F ambient temperatures for both natural gas and distillate fuel oil were used in the modeling to determine the maximum air quality impacts for a range of possible operating conditions.

Six modeling scenarios per fuel type were considered:

1. base operating load for the ambient temperature of 32°F;
2. base operating load for the ambient temperature of 95°F;
3. 75 percent operating load for the ambient temperature of 32°F;
4. 75 percent operating load for the ambient temperature of 95°F;
5. 50 percent operating load for the ambient temperature of 32°F; and

6. 50 percent operating load for the ambient temperature of 95°F.

The proposed CTs will have a stack height of 60 feet and an inner stack diameter of 22 ft.

6.3.5 RECEPTOR LOCATIONS

For predicting maximum concentrations in the vicinity of the plant, a polar receptor grid comprised of 578 grid receptors was used. These receptors included 36 receptors located on radials extending out from the proposed CTs' stack locations. Along each radial, receptors were located at the plant property and distances of 0.1, 0.2, 0.3, 0.5, 0.7, 1.0, 1.5, 2.0, 2.5, 3.0, 4.0, 5.0, 7.0, 10.0, 12.0, and 15.0 km from the proposed CT No 2 stack location. Because of the proximity of the nearest property boundary, the innermost receptor ring distance of 100 m was considered as being ambient air in all directions. In reality, the plant property will extend beyond 100 m in all directions.

Modeling refinements were performed, as needed, by employing a polar receptor grid with a maximum spacing of 100 m along each radial and an angular spacing between radials of 2 degrees.

Since the terrain surrounding the proposed plant site varies little from the stack base elevation of 25 ft above MSL, the terrain was assumed to be flat and receptor elevations were set equal to the stack base elevation.

6.3.6 BUILDING DOWNWASH EFFECTS

The only significant structures in the vicinity of the proposed CT stacks are the proposed CT air filter inlets, CT structure, fuel oil storage tank, and demineralizer water tanks. The height and widths of these structures are as follows:

Structure	Height (ft)	Width (ft)	Length (ft)
CT air inlet	47	24	36
CT structure	22	30	42
Fuel oil tanks	50	100 (diameter)	Not applicable
Demin. water tank		50	100 (diameter) Not applicable

Building dimensions for the project's structures were entered into the EPA's Building Profile Input Program (BPIP, Version 95086) for the purpose of obtaining direction-specific building heights and widths for all downwash-affected sources. The direction-specific building dimensions were then input to the ISCST3 model as the building height and width for each of 36 ten-degree wind sectors. A summary of the direction-specific building dimensions used in the modeling is presented in Appendix C.

6.4 CALPUFF

6.4.1 GENERAL

The CALPUFF long-range transport model was used for refinements in the CNWR for refinements in the significant impact analysis for SO₂. The CNWR is located approximately 139 kilometers (km) to the northwest of the proposed project site. At distances beyond 50 km, the ISCST3 model is considered to overpredict air quality impacts because it is a steady-state model. To provide a more realistic assessment of the project's air quality impacts at the CNWR, a significant impact analysis at the PSD Class I area was performed using the long-range transport model, California Puff model (CALPUFF, Version 5.0).

CALPUFF is not currently a recommended model in EPA's Guideline on Air Quality Models (40 CFR Part 51, Appendix W). However, EPA is planning to formally propose incorporating CALPUFF into Appendix W at the 7th Conference on Air Quality Modeling currently planned for the fall of 1999. In the interim, the Federal Land Managers (FLM) and the Interagency Workgroup on Air Quality Modeling (IWAQM) are recommending the use of CALPUFF for all long-range transport assessments at PSD Class I areas.

A discussion of the CALPUFF model and modeling methodology used for this analysis and the air modeling results is presented in the following sections.

6.4.2 MODEL SELECTION

CALPUFF is a non-steady-state Lagrangian, Gaussian puff model appropriate for simulating air quality impacts over large distances. The model features includes algorithms for simulating plume behavior over complex (i.e., terrain above stack plume height) terrain,

plume transport over water bodies, coastal (i.e., land-sea air) interaction, chemical transformation, and wet and dry deposition and removal. CALPUFF can also incorporate the same building downwash effects, currently used within the ISCST3 model. The model can be used in a screening mode by processing an "enhanced" ISCST3 meteorological data set, or in a refined mode by inputting a three-dimensional meteorological parameter data set generated by the meteorological preprocessor program CALMET. The "enhanced" meteorological data refers to the additional parameters used by the model. These parameters include relative humidity, precipitation, and solar radiation. CALMET produces this data set by inputting various surface, upper air, precipitation, land use, and terrain data over a region and processes this data for a predetermined modeling domain. A postprocessor program called CALPOST processes the CALPUFF-generated concentration or deposition data and produces output of pollutant species concentrations and depositions for various averaging times.

For this analysis, CALPUFF was used in a screening analysis mode, as recommended by the IWAQM Phase 2 Summary Report (12/98). The CALPUFF screening analysis is also referred to as the IWAQM Level II screening analysis or a CALPUFF "light" analysis. The following modeling procedures were used for the Phase II screening analysis.

- Five years of ISCST preprocessed meteorological data. The data set includes the standard ISCST model parameters of wind direction, wind speed, temperature, mixing height and atmospheric stability class, and additional parameters used for dry and wet deposition. These additional parameters include relative humidity, precipitation, and solar radiation.
- Location of receptors in a circle at radials separated by 2-degree intervals. The receptors are located on each radial at a distance that passes through the PSD Class I area. For this analysis, a radius of 139 km was used which is the closest distance from the project site to the CNWR.
- SO₂, use two pollutant species of SO₂ and SO₄
- MESOPUFF II scheme for chemical transformation with CALPUFF default background concentrations of 80 and 10 ppb for ozone and ammonia, respectively
- Both dry and wet deposition and plume depletion
- Modeling domain extends 80 km beyond receptor grid

- Agricultural, unirrigated land use; minimum mixing height of 50 m
- Transitional plume rise, stack-tip downwash, and partial plume penetration
- Puff plume element dispersion (Pasquill-Gifford), rural mode, and ISC building downwash scheme
- Partial plume path adjustment terrain effects
- Highest concentrations predicted in 5 years compared to allowable PSD increments.

6.4.3 BUILDING WAKE EFFECTS

The air modeling analysis included the proposed project's building dimensions to account for the effects of building-induced downwash on the emission sources. The building's dimensions were processed using the Building Profile Input Program (BPIP), Version 95086 and were included in the preliminary ISCST3 modeling analysis.

6.4.4 RECEPTOR LOCATIONS

Receptors were located along a circle that was centered over the project site with a radius equal to the minimum distance to the CNWR (i.e., 139.2 km). The circle contained 180 receptors, equally spaced at 2-degree intervals. A second modeling analysis was performed with 13 receptors located only at the CNWR. Results for both sets of receptors are presented.

6.4.5 METEOROLOGICAL DATA

A 5-year data record was used which consisted of hourly surface observations taken from the National Weather Service (NWS) station at the Tampa International Airport (TPA), coupled with twice-daily mixing height data from the NWS station in Ruskin. The data record was for the years 1987 to 1991. The surface and upper data were preprocessed into an ASCII modeling format by EPA's PCRAMMET meteorological preprocessing program. An anemometer height of 6.7 m was used for the modeling analysis.

Additional meteorological parameters were added to the meteorological data records for use with the CALPUFF model. The addition parameters include:

1. Friction velocity,

2. Monin-Obukhov length,
3. Surface roughness used for calculating dry deposition,
4. Precipitation type code and precipitation rate used for calculating wet deposition,
5. Short-wave solar radiation, and
6. Relative humidity use for calculating chemical transformation rates.

The dry deposition parameters were added to the meteorological data records using the PCRAMMET model in dry deposition mode. Using the guidance provided in Section 3.1 of the PCRAMMET User's Manual (8/98), the following input values were selected:

1. Surface roughness at application site: 0.5 m
2. Surface roughness at the measurement site: 0.03 m,
3. Noontime Albedo: .15,
4. Bowen Ratio: 1.0,
5. Anthropogenic Heat flux: 0,
6. Minimum Monin-Obukhov Length: 25 m, and
7. Fraction of Net Radiation Absorbed by Ground: 0.22.

Hourly precipitation data were obtained from TPA from 1987 to 1991. A precipitation code value was determined for each hour, based on the precipitation classification scheme provided in Table 2-11 of the CALPUFF Users' Manual (7/95). An hour during which no precipitation occurred received a precipitation code value of zero. An hour with precipitation amounts of zero, 0.01 to 0.1, inches, greater than 0.1 to 0.3 inches and greater than 0.3 inches, received precipitation codes of 0, 1, 2, or 3, respectively. These codes are indicative of no, slight, moderate and heavy rain, respectively. Hourly relative humidity and short-wave radiation data were added to the meteorological data record for each of the 5 years. The relative humidity and radiation data were obtained TPA for all years. The addition parameters were obtained from the National Climatic Data Center's Solar and Meteorological Surface Observation Network (SAMSON) and Hourly United States Weather Observations (HUSWO) CDs.

6.4.6 EMISSION INVENTORY

Source parameter and emission rate data used for the CALPUFF modeling analysis are identical to that used in the ISCST3 air modeling analysis.

6.5 AIR MODELING RESULTS

6.5.1 SITE VICINITY

The modeling analysis results for the proposed CTs alone in the vicinity of the plant are summarized in Tables 6-2 through 6-5. The maximum pollutant concentrations predicted in the screening analysis for a single CT and four CTs firing natural gas are presented in Tables 6-2 and 6-3, respectively. Similarly, the maximum pollutant concentrations predicted for one and four CTs firing distillate fuel oil are presented in Tables 6-4 and 6-5, respectively.

As shown in the tables, the maximum predicted PM, SO₂, NO_x and CO impacts due to the proposed CTs are all below the significant impact levels. Because the proposed source will not have a significant impact upon the air quality in the vicinity of the plant site, more detailed modeling analyses for determining compliance with the AAQS and PSD Class II increments are not required.

The maximum predicted PM, SO₂, NO_x, and CO impacts due to the proposed CTs are also below the *de minimis* monitoring levels. Because the proposed source will not have predicted impacts greater than *de minimis* levels, preconstruction monitoring data are not required to be submitted as part of the PSD review.

6.5.2 ISCST3 AT THE CHASSAHOWITZKA NWR PSD CLASS I AREA

The modeling analysis results for the proposed CTs alone at the Chassahowitzka NWR are summarized in Tables 6-6 through 6-9. The maximum pollutant concentrations predicted in the screening analysis for a single CT and four CTs firing natural gas are presented in Tables 6-6 and 6-7, respectively. Similarly, the maximum pollutant concentrations predicted for one and four CTs firing distillate fuel oil are presented in Tables 6-8 and 6-9, respectively.

As shown in the tables, the maximum predicted PM and NO₂ impacts due to the proposed CTs are all below EPA's proposed PSD Class I significant impact levels. Therefore, more

detailed modeling analyses for determining compliance with the AAQS and PSD Class II increments are not required for these pollutants. For SO_2 , the maximum predicted impact from the CTs is above the proposed EPA significant impact levels using the ISCST. Because the proposed plant is approximately 139 km from the PSD Class I area, a more refined dispersion modeling analysis with the CALPUFF long-range transport model is presented to address in greater detail the significance of this pollutant at the PSD Class I area.

A summary of the ISCST3 model results for each year is presented in Appendix D. An example of the model input file is also provided in Appendix D.

6.5.3 CALPUFF AT THE CHASSAHOWITZKA NWR PSD CLASS I AREA

6.5.3.1 Full Circle Receptor Grid

The results of the Level II screening analysis are summarized in Table 6-10. The highest predicted 24-hour concentration is 0.28 ug/m^3 . This concentration occurs in a southerly direction, opposite the direction of the Chassahowitzka NWR. Reviewing the receptors within a 45 degree direction of the Class I area indicated that impacts were less than 0.20 ug/m^3 . Since these impacts occur for the worst-case back-up fuel oil, an evaluation of specific receptors in the Chassahowitzka NWR was performed.

6.5.3.2 Chassahowitzka NWR Receptors

The results of the analysis of specific receptors in the PSD Class I area are summarized in Table 6-10. The highest predicted 24-hour concentration is 0.018 ug/m^3 , which is below the proposed EPA Class I significant impact level of 0.2 ug/m^3 . Taking together, the full circle impacts in the direction to the PSD Class I area, the Class I receptor specific impacts and worst-case nature of the emissions (i.e., fuel oil at a maximum of 1,000 hours), it is concluded that impacts of the proposed are less than the PSD significant impact levels for SO_2 .

Table 6-1. Major Features of the ISCST3 Model

ISCST3 Model Features	
<hr/>	
<ul style="list-style-type: none">• Polar or Cartesian coordinate systems for receptor locations• Rural or one of three urban options which affect wind speed profile exponent, dispersion rates, and mixing height calculations• Plume rise due to momentum and buoyancy as a function of downwind distance for stack emissions (Briggs, 1969, 1971, 1972, and 1975; Bowers, et al., 1979).• Procedures suggested by Huber and Snyder (1976); Huber (1977); and Schulman and Scire (1980) for evaluating building wake effects• Procedures suggested by Briggs (1974) for evaluating stack-tip downwash• Separation of multiple emission sources• Consideration of the effects of gravitational settling and dry deposition on ambient particulate concentrations• Capability of simulating point, line, volume, area, and open pit sources• Capability to calculate dry and wet deposition, including both gaseous and particulate precipitation scavenging for wet deposition• Variation of wind speed with height (wind speed-profile exponent law)• Concentration estimates for 1-hour to annual average times• Terrain-adjustment procedures for elevated terrain including a terrain truncation algorithm for ISCST3; a built-in algorithm for predicting concentrations in complex terrain• Consideration of time-dependent exponential decay of pollutants• The method of Pasquill (1976) to account for buoyancy-induced dispersion• A regulatory default option to set various model options and parameters to EPA recommended values (see text for regulatory options used)• Procedure for calm-wind processing including setting wind speeds less than 1 m/s to 1 m/s.	

Note: ISCST3 = Industrial Source Complex Short-Term.
Source: EPA, 1995.

Table 6.2. Maximum Pollutant Concentrations Predicted for One Proposed Combustion Turbine on Natural Gas at Site Vicinity

Pollutant	Maximum Emission Rates (lb/hr) by Operating Load and Air Temperature						Averaging Time	Maximum Predicted Concentrations (ug/m ³) by Operating Load and Air Temperature (1)					
	Base Load		75% Load		50% Load			Base Load		75% Load		50% Load	
	32°F	95°F	32°F	95°F	32°F	95°F		32°F	95°F	32°F	95°F	32°F	95°F
Generic (10 g/s)	79.37	79.37	79.37	79.37	79.37	79.37	Annual	0.0155	0.0139	0.0180	0.0188	0.0211	0.0219
							24-Hour	0.2010	0.1869	0.2282	0.2431	0.2721	0.2816
							8-Hour	0.4346	0.4019	0.4967	0.5194	0.5811	0.6021
							3-Hour	0.8272	0.8152	0.9713	0.9781	1.1805	1.1894
							1-Hour	1.7828	1.6189	2.1076	2.1854	2.5523	2.5655
SO ₂	5.1	4.6	4.2	3.7	3.4	2.9	Annual	0.001	0.001	0.001	0.001	0.001	0.001
							24-Hour	0.01	0.01	0.01	0.01	0.01	0.01
							3-Hour	0.05	0.05	0.05	0.05	0.05	0.04
NO _x	66.7	59.9	54.4	48.3	43.4	38.3	Annual	0.01	0.01	0.01	0.01	0.01	0.01
PM10	10.0	10.0	10.0	10.0	10.0	10.0	Annual	0.002	0.002	0.002	0.002	0.003	0.003
							24-Hour	0.03	0.02	0.03	0.03	0.03	0.04
CO	44.2	39.3	35.7	32.7	30.0	27.8	8-Hour	0.2	0.2	0.2	0.2	0.2	0.2
							1-Hour	1.0	0.8	0.9	0.9	1.0	0.9

(1) Concentrations are based on highest predicted concentrations using five years of meteorological for 1987 to 1991 of surface and upper air data from the National Weather Service stations at Tampa International Airport and Ruskin, respectively.

Table 6-3. Maximum Pollutant Concentrations Predicted for Four Simple-Cycle Combustion Turbines on Natural Gas Compared to EPA Significant Impact Levels

Pollutant	Averaging Time	Maximum Predicted Concentrations (ug/m³) by Operating Load and Air Temperature (1)						EPA Significant Impact Levels (ug/m³)
		Base Load		75% Load		50% Load		
		32°F	95°F	32°F	95°F	32°F	95°F	
SO₂	Annual	0.004	0.003	0.004	0.004	0.004	0.003	1
	24-Hour	0.05	0.04	0.05	0.05	0.05	0.04	5
	3-Hour	0.21	0.19	0.21	0.18	0.20	0.17	25
NOₓ	Annual	0.052	0.042	0.049	0.046	0.046	0.042	1
PM10	Annual	0.008	0.007	0.009	0.009	0.011	0.011	1
	24-Hour	0.10	0.09	0.12	0.12	0.14	0.14	5
CO	8-Hour	1	1	1	1	1	1	500
	1-Hour	4	3	4	4	4	4	2,000

(1) Concentrations are based on highest predicted concentrations using five years of meteorological for 1987 to 1991 of surface and upper air data from the National Weather Service stations at Tampa International Airport and Ruskin, respectively.

Table 6-4. Maximum Pollutant Concentrations Predicted for One Proposed Combustion Turbine on Fuel Oil at Site Vicinity

Pollutant	Maximum Emission Rates (lb/hr) by Operating Load and Air Temperature						Averaging Time	Maximum Predicted Concentrations (ug/m ³) by Operating Load and Air Temperature (1)					
	Base Load		75% Load		50% Load			Base Load		75% Load		50% Load	
	32°F	95°F	32°F	95°F	32°F	95°F		32°F	95°F	32°F	95°F	32°F	95°F
Generic (10 g/s)	79.37	79.37	79.37	79.37	79.37	79.37	Annual	0.0151	0.0159	0.0179	0.0186	0.0207	0.0216
							24-Hour	0.1968	0.2053	0.2272	0.2393	0.2657	0.2784
							8-Hour	0.4249	0.4446	0.4945	0.5107	0.5682	0.5951
							3-Hour	0.8239	0.9546	0.9706	0.9755	1.1742	1.1863
							1-Hour	1.7308	1.8362	2.1061	2.1679	2.5098	2.5609
SO ₂	101.5	93.4	82.6	74.8	65.6	58.9	Annual	0.019	0.019	0.019	0.018	0.017	0.016
							24-Hour	0.25	0.24	0.24	0.23	0.22	0.21
							3-Hour	1.05	1.12	1.01	0.92	0.97	0.88
NO _x	362.0	335.8	296.7	267.8	236.4	209.3	Annual	0.07	0.07	0.07	0.06	0.06	0.06
PM10	17.0	17.0	17.0	17.0	17.0	17.0	Annual	0.003	0.003	0.004	0.004	0.004	0.005
							24-Hour	0.04	0.04	0.05	0.05	0.06	0.06
CO	74.4	66.2	57.6	53.9	72.2	67.5	8-Hour	0.4	0.4	0.4	0.3	0.5	0.5
							1-Hour	1.6	1.5	1.5	1.5	2.3	2.2

(1) Concentrations are based on highest predicted concentrations using five years of meteorological for 1987 to 1991 of surface and upper air data from the National Weather Service stations at Tampa International Airport and Ruskin, respectively.

Pollutant concentrations were based on a modeled or generic concentration predicted using a modeled emission rate of 79.37 lb/hr (10 g/s). Specific pollutant concentrations were estimated by multiplying the modeled concentration (at 10 g/s) by the ratio of the specific pollutant to the modeled emission rate of 10 g/s.

$$\frac{79.37}{X} = 1 \quad \frac{101.5}{Y} = 2$$

$$1.0067$$

Table 6-5. Maximum Pollutant Concentrations Predicted for Four Simple-Cycle Combustion Turbines on Fuel Oil
Compared to EPA Significant Impact Levels

Pollutant	Averaging Time	Maximum Predicted Concentrations (ug/m ³) by Operating Load and Air Temperature (1)						EPA Significant Impact Levels (ug/m ³)
		Base Load		75% Load		50% Load		
		32°F	95°F	32°F	95°F	32°F	95°F	
SO ₂	Annual	0.08	0.07	0.07	0.07	0.07	0.06	1
	24-Hour	1.0	1.0	0.9	0.9	0.9	0.8	5
	3-Hour	4	4	4	4	4	4	25
NO _x	Annual	0.3	0.3	0.3	0.3	0.2	0.2	1
PM10	Annual	0.01	0.01	0.02	0.02	0.02	0.02	1
	24-Hour	0.2	0.2	0.2	0.2	0.2	0.2	5
CO	8-Hour	2	1	1	1	2	2	500
	1-Hour	6	6	6	6	9	9	2,000

(1) Concentrations are based on highest predicted concentrations using five years of meteorological for 1987 to 1991
of surface and upper air data from the National Weather Service stations at Tampa International Airport and Ruskin, respecti

Table 6-4 X4

Table 6-6. Maximum Pollutant Concentrations Predicted for One Proposed Combustion Turbine on Natural Gas at Chassahowitzka NWA PSD Class I Area Using ISCST3

Pollutant	Maximum Emission Rates (lb/hr) by Operating Load and Air Temperature						Averaging Time	Maximum Predicted Concentrations (ug/m ³) by Operating Load and Air Temperature (1)					
	Base Load		75% Load		50% Load			Base Load		75% Load		50% Load	
	32°F	95°F	32°F	95°F	32°F	95°F		32°F	95°F	32°F	95°F	32°F	95°F
Generic (10 g/s)	79.37	79.37	79.37	79.37	79.37	79.37	Annual	0.0026	0.0024	0.0029	0.0030	0.0035	0.0035
							24-Hour	0.0521	0.0485	0.0589	0.0613	0.0679	0.0698
							8-Hour	0.1563	0.1452	0.1766	0.1840	0.2036	0.2094
							3-Hour	0.2511	0.2410	0.2682	0.2740	0.3014	0.3115
							1-Hour	0.5120	0.4852	0.5586	0.5748	0.6173	0.6294
SO ₂	5.1	4.6	4.2	3.7	3.4	2.9	Annual	0.0002	0.0001	0.0002	0.0001	0.0001	0.0001
							24-Hour	0.003	0.003	0.003	0.003	0.003	0.003
							3-Hour	0.02	0.01	0.01	0.01	0.01	0.01
NO _x	66.7	59.9	54.4	48.3	43.4	38.3	Annual	0.002	0.002	0.002	0.002	0.002	0.002
PM10	10.0	10.0	10.0	10.0	10.0	10.0	Annual	0.0003	0.0003	0.0004	0.0004	0.0004	0.0004
							24-Hour	0.01	0.01	0.01	0.01	0.01	0.01
CO	44.2	39.3	35.7	32.7	30.0	27.8	8-Hour	0.1	0.1	0.1	0.1	0.1	0.1
							1-Hour	0.3	0.2	0.3	0.2	0.2	0.2

(1) Concentrations are based on highest predicted concentrations using five years of meteorological for 1987 to 1991 of surface and upper air data from the National Weather Service stations at Tampa International Airport and Ruskin, respectively.

Pollutant concentrations were based on a modeled or generic concentration predicted using a modeled emission rate of 79.37 lb/hr (10 g/s). Specific pollutant concentrations were estimated by multiplying the modeled concentration (at 10 g/s) by the ratio of the specific pollutant emission rate to the modeled emission rate of 10 g/s.

Table 6-7. Maximum Pollutant Concentrations Predicted for Four Simple-Cycle Combustion Turbines on Natural Gas Compared to Proposed EPA PSD Class I Significant Impact Levels Using ISCST3

Pollutant	Averaging Time	Maximum Predicted Concentrations (ug/m³) by Operating Load and Air Temperature (1)						Proposed EPA Class I Significant Impact Levels (ug/m³)
		Base Load		75% Load		50% Load		
		32°F	95°F	32°F	95°F	32°F	95°F	
SO₂	Annual	0.0007	0.0006	0.0006	0.0006	0.0006	0.0005	0.1
	24-Hour	0.013	0.011	0.012	0.011	0.012	0.010	0.2
	3-Hour	0	0.1	0.1	0.1	0.1	0.0	1.0
NOₓ	Annual	0.01	0.007	0.008	0.007	0.008	0.007	0.1
PM10	Annual	0.00	0.001	0.001	0.002	0.002	0.002	0.2
	24-Hour	0.0	0.02	0.03	0.03	0.03	0.04	0.3

(1) Concentrations are based on highest predicted concentrations using five years of meteorological for 1987 to 1991 of surface and upper air data from the National Weather Service stations at Tampa International Airport and Ruskin, respectively

Table 6-8. Maximum Pollutant Concentrations Predicted for One Proposed Combustion Turbine on Fuel Oil
at the Chassahowitzka PSD Class I Area Using ISCST3

Pollutant	Maximum Emission Rates (lb/hr) by Operating Load and Air Temperature						Averaging Time	Maximum Predicted Concentrations (ug/m ³) by Operating Load and Air Temperature (1)					
	Base Load		75% Load		50% Load			Base Load		75% Load		50% Load	
	32°F	95°F	32°F	95°F	32°F	95°F		32°F	95°F	32°F	95°F	32°F	95°F
Generic (10 g/s)	79.37	79.37	79.37	79.37	79.37	79.37	Annual	0.0025	0.0026	0.0029	0.0030	0.0034	0.0035
							24-Hour	0.0510	0.0532	0.0586	0.0604	0.0665	0.0692
							8-Hour	0.1531	0.1506	0.1759	0.1812	0.1995	0.2075
							3-Hour	0.2482	0.2539	0.2676	0.2718	0.2942	0.3081
							1-Hour	0.5044	0.5196	0.5570	0.5686	0.6085	0.6253
SO ₂	101.5	93.4	82.6	74.8	65.6	58.9	Annual	0.003	0.003	0.003	0.003	0.003	0.003
							24-Hour	0.07	0.06	0.06	0.06	0.05	0.05
							3-Hour	0.32	0.30	0.28	0.26	0.24	0.23
NO _x	362.0	335.8	296.7	267.8	236.4	209.3	Annual	0.01	0.01	0.01	0.01	0.01	0.01
PM10	17.0	17.0	17.0	17.0	17.0	17.0	Annual	0.001	0.001	0.001	0.001	0.001	0.001
							24-Hour	0.01	0.01	0.01	0.01	0.01	0.01
CO	74.4	66.2	57.6	53.9	72.2	67.5	8-Hour	0.1	0.1	0.1	0.1	0.2	0.2
							1-Hour	0.5	0.4	0.4	0.4	0.6	0.5

(1) Concentrations are based on highest predicted concentrations using five years of meteorological for 1987 to 1991
of surface and upper air data from the National Weather Service stations at Tampa International Airport and Ruskin, respectively.

Pollutant concentrations were based on a modeled or generic concentration predicted using a modeled emission rate of 79.37 lb/hr (10 g/s).
Specific pollutant concentrations were estimated by multiplying the modeled concentration (at 10 g/s) by the ratio of the specific pollutant emission rate
to the modeled emission rate of 10 g/s.

Table 6-9. Maximum Pollutant Concentrations Predicted for Four Simple-Cycle Combustion Turbines on Fuel Oil
Compared to Proposed EPA PSD Class I Significant Impact Levels Using ISCST3

Pollutant	Averaging Time	Maximum Predicted Concentrations (ug/m ³) by Operating Load and Air Temperature (1)						Proposed EPA Class I Significant Impact Levels (ug/m ³)
		Base Load		75% Load		50% Load		
		32°F	95°F	32°F	95°F	32°F	95°F	
SO ₂	Annual	0.013	0.012	0.012	0.011	0.011	0.010	0.1
	24-Hour	0.26	0.25	0.24	0.23	0.22	0.21	0.2
	3-Hour	1.3	1.2	1.1	1.0	1.0	0.9	1.0
NO _x	Annual	0.05	0.04	0.04	0.04	0.04	0.04	0.1
PM10	Annual	0.002	0.002	0.002	0.003	0.003	0.003	0.2
	24-Hour	0.04	0.05	0.05	0.05	0.06	0.06	0.3

(1) Concentrations are based on highest predicted concentrations using five years of meteorological for 1987 to 1991 of surface and upper air data from the National Weather Service stations at Tampa International Airport and Ruskin, respectively.

Table 6-10. Maximum 24-Hour SO₂ Concentration Predicted for the Four Combustion Turbines at the Chassahowitzka National Wildlife Refuge (NWR), Refined SO₂ Significant Impact Analysis Using CALPUFF

Concentration Rank	Year	Receptor Distance at 139 km Ring		Chassahowitzka NWR (Proposed EPA PSD Class I Significant Impact Level (ug/m ³)
		Concentration (ug/m ³)	Julian Day	Concentration (ug/m ³)	Julian Day	
High	1987	0.25	285	0.122	229	0.2
	1988	0.26	281	0.132	21	0.2
	1989	0.28	338	0.153	343	0.2
	1990	0.24	263	0.177	47	0.2
	1991	0.24	351	0.095	73	0.2

(1) Concentrations predicted with CALPUFF model with ISCST meteorological data from the National Weather Service (NWS) stations from Tampa and Tampa (surface) and Ruskin (upper air) for 1987 to 1991. See text for details.

For receptor distance at 139 km ring, concentrations were predicted along a circle with a radius equal to the minimum distance to the Class I area (i.e., 139 km). The circle contained 180 receptors, spaced at 2-degree intervals. Concentrations were also predicted at 13 receptors located at the Chassahowitzka NWR.

7.0 ADDITIONAL IMPACT ANALYSIS

7.1 IMPACTS DUE TO DIRECT GROWTH

The proposed project is being constructed to meet peaking electric demands. Additional growth as a direct result of the additional electric power provided by the project is not expected. The project will be constructed and operated with minimum labor and associated facilities and is not expected to significantly affect growth in the area. As a result, air pollution impacts from additional growth are not anticipated.

7.2 IMPACT ON SOILS, VEGETATION AND WILDLIFE

Because the proposed project's impacts on the local air quality are predicted to be less than the significant impact levels for PSD Class II areas, the project's impacts on soils, vegetation, and wildlife are also not expected to be significant.

7.3 IMPACTS UPON PSD CLASS I AREAS

The proposed project is located approximately 139 km from the Chassahowitzka NWR, the nearest PSD Class I area. The air quality impact evaluation for the project indicate that pollutant concentrations will not be significant at the distance of the Class I area. Because the proposed CTs will be fired primarily with natural gas, a clean fuel, it is expected that the project's impacts for SO₂, NO₂, and PM₁₀ will be minimal and not significantly affect or impair visibility or soils and vegetation at the Class I areas.

APPENDIX A

EXPECTED PERFORMANCE AND EMISSION INFORMATION ON "F" CLASS COMBUSTION TURBINE

(Note: SO₂ based on 0.2 gr/100 cf of H₂S. Actual total sulfur based on 1 gr/100 cf to account for odorant (mercaptans) in pipeline gas.)

Table A-1. Design Information and Stack Parameters for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Natural Gas, Base Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Combustion Turbine Performance			
Net power output (MW)	179.2	172.2	156.6
Net heat rate (Btu/kWh, LHV)	9,319	9,361	9,591
(Btu/kWh, HHV)	10,344	10,391	10,646
Heat Input (MMBtu/hr, LHV)	1,670	1,612	1,502
(MMBtu/hr, HHV)	1,854	1,789	1,667
Fuel heating value (Btu/lb, LHV)	20,751	20,751	20,751
(Btu/lb, HHV)	23,006	23,006	23,006
(HHV/LHV)	1.110	1.110	1.110
CT Exhaust Flow			
Mass Flow (lb/hr)- with margin of 10%	4,063,400	3,919,300	3,672,900
- provided	3,694,000	3,563,000	3,339,000
Temperature (°F)	1,097	1,113	1,135
Moisture (% Vol.)	7.9	8.6	10.3
Oxygen (% Vol.)	12.60	12.50	12.20
Molecular Weight	28.44	28.34	28.16
Fuel Usage			
Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu (Fuel Heat Content, Btu/lb (LHV))			
Heat input (MMBtu/hr, LHV)	1,670	1,612	1,502
Heat content (Btu/lb, LHV)	20,751	20,751	20,751
Fuel usage (lb/hr)- calculated	80,478	77,683	72,382
CT Stack			
CT- Stack height (ft)	60	60	60
Diameter (ft)	22	22	22
Turbine Flow Conditions (CT Stack-Unit 4 only)			
Turbine Flow (acfm) = [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F) + 460°F)] / [Molecular weight x 2116.8] / 60 min/hr			
Mass flow (lb/hr)	4,063,400	3,919,300	3,672,900
Temperature (°F)	1,097	1,113	1,135
Molecular weight	28.44	28.34	28.16
Volume flow (acfm)- calculated	2,706,395	2,645,986	2,530,918
(ft ³ /s)- calculated	45,107	44,100	42,182
Velocity (ft/sec)	118.7	116.0	111.0

Note: Universal gas constant = 1,545 ft-lb(force)/°R; atmospheric pressure = 2,116.8 lb(force)/ft²; 14.7 lb/ft²

Source: GE, 1998.

Table A-2. Maximum Emissions for Criteria Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Natural Gas, Base Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	3,390	3,390	3,390
Particulate (lb/hr) = Emission rate (lb/hr) from manufacturer			
Basis (excludes H ₂ SO ₄), lb/hr	10	10	10
Emission rate (lb/hr)- provided	10.0	10.0	10.0
(TPY)	17.0	17.0	17.0
Sulfur Dioxide (lb/hr) = Natural gas (cf/hr) x sulfur content (gr/100 cf) x 1 lb/7000 gr x (lb SO ₂ /lb S)/100			
Fuel density (lb/ft ³)	0.0448	0.0448	0.0448
Fuel use (cf/hr)	1,797,031	1,734,619	1,616,252
Sulfur content (grains/ 100 cf)	1	1	1
lb SO ₂ /lb S (64/32)	2	2	2
Emission rate (lb/hr)	5.1	5.0	4.6
(TPY)	8.70	8.40	7.83
Nitrogen Oxides (lb/hr) = NOx(ppm) x {[20.9 x (1 - Moisture(%)/100)] - Oxygen(%)} x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]			
Basis, ppmvd @15% O ₂	9	9	9
Moisture (%)	7.9	8.6	10.3
Oxygen (%)	12.6	12.5	12.2
Turbine Flow (acfm)	2,706,395	2,645,986	2,530,918
Turbine Exhaust Temperature (°F)	1,097	1,113	1,135
Emission rate (lb/hr)	66.7	64.1	59.9
(TPY)	113.0	108.6	101.6
Carbon Monoxide (lb/hr) = CO(ppm) x [1 - Moisture(%)/100] x 2116.8 lb/ft ² x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]			
Basis, ppmvd	12	12	12
Moisture (%)	7.9	8.6	10.3
Turbine Flow (acfm)	2,706,395	2,645,986	2,530,918
Turbine Exhaust Temperature (°F)	1,097	1,113	1,135
Emission rate (lb/hr)	44.2	42.5	39.3
(TPY)	75.0	72.0	66.6
VOCs (lb/hr) = VOC(ppmvd) x [1-Moisture(%)/100] x 2116.8 lb/ft ² x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]			
Basis, ppmvd	1.4	1.4	1.4
Moisture (%)	7.9	8.6	10.3
Turbine Flow (acfm)	2,706,395	2,645,986	2,530,918
Turbine Exhaust Temperature (°F)	1,097	1,113	1,135
Emission rate (lb/hr)	2.95	2.83	2.62
(TPY)	5.0	4.8	4.4
Lead (lb/hr) = NA			
Emission Rate Basis	NA	NA	NA
Emission rate (lb/hr)	NA	NA	NA
(TPY)	NA	NA	NA

Note: ppmvd = parts per million, volume dry; O₂ = oxygen.

Source: GE, 1998; Colder Associates, 1998; EPA, 1996

Table A-3. Maximum Emissions for Other Regulated PSD Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Natural Gas, Base Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	3,390	3,390	3,390
$2,3,7,8 \text{ TCDD Equivalents (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a) , lb/10 ¹² Btu	1.20E-06	1.20E-06	0.00E+00
Heat Input Rate (MMBtu/hr)	1.85E+03	1.79E+03	1.67E+03
Emission Rate (lb/hr)	2.22E-09	2.15E-09	0.00E+00
(TPY)	3.77E-09	3.64E-09	0.00E+00
$\text{Beryllium (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a) , lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,854	1,789	1,667
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
$\text{Fluoride (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (b) , lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,854	1,789	1,667
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
$\text{Mercury (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a) , lb/10 ¹² Btu	7.48E-04	7.48E-04	7.48E-04
Heat Input Rate (MMBtu/hr)	1,854	1,789	1,667
Emission Rate (lb/hr)	1.39E-06	1.34E-06	1.25E-06
(TPY)	2.35E-06	2.27E-06	2.11E-06
$\text{Sulfuric Acid Mist} = \text{Fuel Use (lb/hr)} \times \text{sulfur (S) content (fraction)} \times \text{conversion of S to H}_2\text{SO}_4 \text{ (\%)} \\ \times \text{MW H}_2\text{SO}_4 / \text{MW S (98/32)}$			
Fuel Usage (cf/hr)	1,797,031	1,734,619	1,616,252
Sulfur (lb/hr)	2.57	2.48	2.31
lb H ₂ SO ₄ / lb S (98/32)	3.0625	3.0625	3.0625
Conversion to H ₂ SO ₄ (%) (c)	10	10	10
Emission Rate (lb/hr)	0.79	0.76	0.71
(TPY)	1.33	1.29	1.20

Sources: (a) Golder Associates, 1998; (b) EPA, 1981; (c) Assumed.

Note: No Emission Factors for Hydrogen chloride (HCl) from natural gas firing.

Table A-4. Maximum Emissions for Hazardous Air Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Natural Gas, Base Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	3,390	3,390	3,390
Antimony (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0.00E+00	0.00E+00	0.00E+00
Heat Input Rate (MMBtu/hr)	1,854	1,789	1,667
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Benzene (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0.8	0.8	0.8
Heat Input Rate (MMBtu/hr)	1,854	1,789	1,667
Emission Rate (lb/hr)	1.48E-03	1.43E-03	1.33E-03
(TPY)	2.51E-03	2.43E-03	2.26E-03
Cadmium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,854	1,789	1,667
Emission Rate (lb/hr)	0	0	0
(TPY)	0.00E+00	0.00E+00	0.00E+00
Chromium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,854	1,789	1,667
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Formaldehyde (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	34	34	34
Heat Input Rate (MMBtu/hr)	1,854	1,789	1,667
Emission Rate (lb/hr)	6.30E-02	6.08E-02	5.67E-02
(TPY)	1.07E-01	1.03E-01	9.61E-02
Cobalt (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1.85E+03	1.79E+03	1.67E+03
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00
(TPY)	0	0	0
Manganese (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,854	1,789	1,667
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Nickel (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,854	1,789	1,667
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Phosphorous (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (b), lb/10 ¹² Btu	0.00E+00	0.00E+00	0.00E+00
Heat Input Rate (MMBtu/hr)	1,854	1,789	1,667
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Selenium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,854	1,789	1,667
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Toluene (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	10	10	10
Heat Input Rate (MMBtu/hr)	1,854	1,789	1,667
Emission Rate (lb/hr)	1.85E-02	1.79E-02	1.67E-02
(TPY)	3.14E-02	3.03E-02	2.83E-02

Sources: (a) Golder Associates, 1998; (b) EPA, 1996 (AP-42, Table 3.1-4)

Table A-5. Design Information and Stack Parameters for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Natural Gas, 75% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Combustion Turbine Performance			
Net power output (MW)	134.2	126.4	111.1
Net heat rate (Btu/kWh, LHV)	10,261	10,396	10,882
(Btu/kWh, HHV)	11,045	11,289	11,765
Heat Input (MMBtu/hr, LHV)	1,377	1,314	1,209
(MMBtu/hr, HHV)	1,482	1,427	1,307
Fuel heating value (Btu/lb, LHV)	20,751	20,751	20,751
(Btu/lb, HHV)	23,006	23,006	23,006
(HHV/LHV)	1.110	1.110	1.110
CT Exhaust Flow			
Mass Flow (lb/hr)- with margin of 10%	3,285,700	3,190,000	3,039,300
- provided	2,987,000	2,900,000	2,763,000
Temperature (°F)	1,170	1,179	1,193
Moisture (% Vol.)	8.1	8.4	9.6
Oxygen (% Vol.)	12.50	12.50	12.50
Molecular Weight	28.41	28.38	28.21
Fuel Usage			
Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu (Fuel Heat Content, Btu/lb (LHV))			
Heat input (MMBtu/hr, LHV)	1,377	1,314	1,209
Heat content (Btu/lb, LHV)	20,751	20,751	20,751
Fuel usage (lb/hr)- calculated	66,358	63,322	58,262
CT Stack			
CT- Stack height (ft)	60	60	60
Diameter (ft)	22	22	22
Turbine Flow Conditions (CT Stack-Unit 4 only)			
Turbine Flow (acfm) = [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F) + 460°F)] / [Molecular weight x 2116.8] / 60 min/hr			
Mass flow (lb/hr)	3,285,700	3,190,000	3,039,300
Temperature (°F)	1,170	1,179	1,193
Molecular weight	28.41	28.38	28.21
Volume flow (acfm)- calculated	2,292,951	2,240,823	2,166,041
(ft ³ /s)- calculated	38,216	37,347	36,101
Velocity (ft/sec)	100.5	98.2	95.0

Note: Universal gas constant = 1,545 ft-lb(force)/°R; atmospheric pressure = 2,116.8 lb(force)/ft²; 14.7 lb/ft³

Source: GE, 1998.

Table A-6. Maximum Emissions for Criteria Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Natural Gas, 75% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	3,390	3,390	3,390
Particulate (lb/hr) = Emission rate (lb/hr) from manufacturer			
Basis (excludes H ₂ SO ₄), lb/hr	10	10	10
Emission rate (lb/hr) - provided	10.0	10.0	10.0
(TPY)	17.0	17.0	17.0
Sulfur Dioxide (lb/hr) = Natural gas (cf/hr) x sulfur content (gr/100 cf) x 1 lb/7000 gr x (lb SO ₂ /lb S)/100			
Fuel density (lb/ft ³)	0.0448	0.0448	0.0448
Fuel use (cf/hr)	1,481,744	1,413,951	1,300,964
Sulfur content (grains/100 cf)	1	1	1
lb SO ₂ /lb S (64/32)	2	2	2
Emission rate (lb/hr)	4.2	4.0	3.7
(TPY)	7.18	6.85	6.30
Nitrogen Oxides (lb/hr) = NOx(ppm) x [(20.9 x (1 - Moisture(%)/100)) - Oxygen(%)] x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]			
Basis, ppmvd @15% O ₂	9	9	9
Moisture (%)	8.1	8.4	9.6
Oxygen (%)	12.5	12.5	12.5
Turbine Flow (acfm)	2,292,951	2,240,823	2,166,041
Turbine Exhaust Temperature (°F)	1,170	1,179	1,193
Emission rate (lb/hr)	54.4	52.4	48.3
(TPY)	92.2	88.8	81.9
Carbon Monoxide (lb/hr) = CO(ppm) x [1 - Moisture(%)/100] x 2116.8 lb/ft ² x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]			
Basis, ppmvd	12	12	12
Moisture (%)	8.1	8.4	9.6
Turbine Flow (acfm)	2,292,951	2,240,823	2,166,041
Turbine Exhaust Temperature (°F)	1,170	1,179	1,193
Emission rate (lb/hr)	35.7	34.6	32.7
(TPY)	60.5	58.6	55.5
VOCs (lb/hr) = VOC(ppmvd) x [1 - Moisture(%)/100] x 2116.8 lb/ft ² x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]			
Basis, ppmvd	1.4	1.4	1.4
Moisture (%)	8.1	8.4	9.6
Turbine Flow (acfm)	2,292,951	2,240,823	2,166,041
Turbine Exhaust Temperature (°F)	1,170	1,179	1,193
Emission rate (lb/hr)	2.38	2.31	2.18
(TPY)	4.0	3.9	3.7
Lead (lb/hr) = NA			
Emission Rate Basis	NA	NA	NA
Emission rate (lb/hr)	NA	NA	NA
(TPY)	NA	NA	NA

Note: ppmvd = parts per million, volume dry; O₂ = oxygen.

Source: GE, 1998; Golder Associates, 1998; EPA, 1996

Table A-7. Maximum Emissions for Other Regulated PSD Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Natural Gas, 75% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	3,390	3,390	3,390
$2,3,7,8\text{-TCDD Equivalents (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a) , lb/10 ¹² Btu	1.20E-06	1.20E-06	1.20E-06
Heat Input Rate (MMBtu/hr)	1.48E+03	1.43E+03	1.31E+03
Emission Rate (lb/hr)	1.78E-09	1.71E-09	1.57E-09
(TPY)	3.01E-09	2.90E-09	2.66E-09
$\text{Beryllium (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a) , lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,482	1,427	1,307
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
$\text{Fluoride (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (b) , lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,482	1,427	1,307
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
$\text{Mercury (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a) , lb/10 ¹² Btu	7.48E-04	7.48E-04	7.48E-04
Heat Input Rate (MMBtu/hr)	1,482	1,427	1,307
Emission Rate (lb/hr)	1.11E-06	1.07E-06	9.78E-07
(TPY)	1.88E-06	1.81E-06	1.66E-06
$\text{Sulfuric Acid Mist} = \text{Fuel Use (lb/hr)} \times \text{sulfur (S) content (fraction)} \times \text{conversion of S to H}_2\text{SO}_4 \text{ (\%)} \times \text{MW H}_2\text{SO}_4 / \text{MW S (98/32)}$			
Fuel Usage (cf/hr)	1,481,744	1,413,951	1,300,964
Sulfur (lb/hr)	2.12	2.02	1.86
lb H ₂ SO ₄ / lb S (98/32)	3.0625	3.0625	3.0625
Conversion to H ₂ SO ₄ (%) (c)	10	10	10
Emission Rate (lb/hr)	0.65	0.62	0.57
(TPY)	1.10	1.05	0.96

Sources: (a) Golder Associates, 1998; (b) EPA, 1981; (c) Assumed.

Table A-8. Maximum Emissions for Hazardous Air Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Natural Gas, 75% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	3,390	3,390	3,390
Antimony (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0.00E+00	0.00E+00	0.00E+00
Heat Input Rate (MMBtu/hr)	1,482	1,427	1,307
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Benzene (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0.8	0.8	0.8
Heat Input Rate (MMBtu/hr)	1,482	1,427	1,307
Emission Rate (lb/hr)	1.19E-03	1.14E-03	1.05E-03
(TPY)	2.01E-03	1.93E-03	1.77E-03
Cadmium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,482	1,427	1,307
Emission Rate (lb/hr)	0	0	0
(TPY)	0.00E+00	0.00E+00	0.00E+00
Chromium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,482	1,427	1,307
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Formaldehyde (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	34	34	34
Heat Input Rate (MMBtu/hr)	1,482	1,427	1,307
Emission Rate (lb/hr)	5.04E-02	4.85E-02	4.44E-02
(TPY)	8.54E-02	8.22E-02	7.53E-02
Cobalt (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1.48E+03	1.43E+03	1.31E+03
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00
(TPY)	0	0	0
Manganese (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,482	1,427	1,307
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Nickel (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,482	1,427	1,307
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Phosphorous (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (b), lb/10 ¹² Btu	0.00E+00	0.00E+00	0.00E+00
Heat Input Rate (MMBtu/hr)	1,482	1,427	1,307
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Selenium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,482	1,427	1,307
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Toluene (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	10	10	10
Heat Input Rate (MMBtu/hr)	1,482	1,427	1,307
Emission Rate (lb/hr)	1.48E-02	1.43E-02	1.31E-02
(TPY)	2.51E-02	2.42E-02	2.22E-02

Sources: (a) Golder Associates, 1998; (b) EPA, 1996 (AP-42, Table 3.1-4)

Table A-9. Design Information and Stack Parameters for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Natural Gas, 50% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Combustion Turbine Performance			
Net power output (MW)	90.76	85.55	74.6
Net heat rate (Btu/kWh, LHV)	12,054	12,086	12,842
(Btu/kWh, HHV)	13,380	13,416	14,254
Heat Input (MMBtu/hr, LHV)	1,094	1,034	958
(MMBtu/hr, HHV)	1,214	1,148	1,063
Fuel heating value (Btu/lb, LHV)	20,751	20,751	20,751
(Btu/lb, HHV)	23,006	23,006	23,006
(HHV/LHV)	1.110	1.110	1.110
CT Exhaust Flow			
Mass Flow (lb/hr)- with margin of 10%	2,754,400	2,654,300	2,570,700
- provided	2,504,000	2,413,000	2,337,000
Temperature (°F)	1,171	1,186	1,200
Moisture (% Vol.)	7.7	8	9.1
Oxygen (% Vol.)	12.90	13.00	13.00
Molecular Weight	28.44	28.41	28.26
Fuel Usage			
Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu (Fuel Heat Content, Btu/lb (LHV))			
Heat input (MMBtu/hr, LHV)	1,094	1,034	958
Heat content (Btu/lb, LHV)	20,751	20,751	20,751
Fuel usage (lb/hr)- calculated	52,720	49,829	46,166
CT Stack			
CT- Stack height (ft)	60	60	60
Diameter (ft)	22	22	22
Turbine Flow Conditions (CT Stack-Unit 4 only)			
Turbine Flow (acfm) = [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F) + 460°F)] / [Molecular weight x 2116.8] / 60 min/hr			
Mass flow (lb/hr)	2,754,400	2,654,300	2,570,700
Temperature (°F)	1,171	1,186	1,200
Molecular weight	28.44	28.41	28.26
Volume flow (acfm)- calculated	1,921,470	1,870,642	1,836,829
(ft ³ /s)- calculated	32,024	31,177	30,614
Velocity (ft/sec)	84.2	82.0	80.5

Note: Universal gas constant = 1,545 ft-lb(force)/°R; atmospheric pressure = 2,116.8 lb(force)/ft²; 14.7 lb/ft³

Source: GE, 1998.

Table A-10. Maximum Emissions for Criteria Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NO_x Combustor, Natural Gas, 50% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	3,390	3,390	3,390
Particulate (lb/hr) = Emission rate (lb/hr) from manufacturer			
Basis (excludes H ₂ SO ₄), lb/hr	10	10	10
Emission rate (lb/hr)- provided	10.0	10.0	10.0
(TPY)	17.0	17.0	17.0
Sulfur Dioxide (lb/hr) = Natural gas (cf/hr) x sulfur content(gr/100 cf) x 1 lb/7000 gr x (lb SO ₂ /lb S)/100			
Fuel density (lb/ft ³)	0.0448	0.0448	0.0448
Fuel use (cf/hr)	1,177,217	1,112,653	1,030,872
Sulfur content (grains/ 100 cf)	1	1	1
lb SO ₂ /lb S (64/32)	2	2	2
Emission rate (lb/hr)	3.4	3.2	2.9
(TPY)	5.70	5.39	4.99
Nitrogen Oxides (lb/hr) = NO _x (ppm) x {[20.9 x (1 - Moisture(%)/100)] - Oxygen(%)} x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NO _x) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]			
Basis, ppmvd @15% O ₂	9	9	9
Moisture (%)	7.7	8	9.1
Oxygen (%)	12.9	13	13
Turbine Flow (acfm)	1,921,470	1,870,642	1,836,829
Turbine Exhaust Temperature (°F)	1,171	1,186	1,200
Emission rate (lb/hr)	43.4	40.8	38.3
(TPY)	73.6	69.2	64.9
Carbon Monoxide (lb/hr) = CO(ppm) x [1 - Moisture(%)/100] x 2116.8 lb/ft ² x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]			
Basis, ppmvd	12	12	12
Moisture (%)	7.7	8	9.1
Turbine Flow (acfm)	1,921,470	1,870,642	1,836,829
Turbine Exhaust Temperature (°F)	1,171	1,186	1,200
Emission rate (lb/hr)	30.0	28.9	27.8
(TPY)	50.9	49.0	47.1
VOCs (lb/hr) = VOC(ppmvd) x [1-Moisture(%)/100] x 2116.8 lb/ft ² x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]			
Basis, ppmvd	1.4	1.4	1.4
Moisture (%)	7.7	8	9.1
Turbine Flow (acfm)	1,921,470	1,870,642	1,836,829
Turbine Exhaust Temperature (°F)	1,171	1,186	1,200
Emission rate (lb/hr)	2.00	1.93	1.85
(TPY)	3.4	3.3	3.1
Lead (lb/hr)= NA			
Emission Rate Basis	NA	NA	NA
Emission rate (lb/hr)	NA	NA	NA
(TPY)	NA	NA	NA

Note: ppmvd= parts per million, volume dry; O₂= oxygen.

Source: GE, 1998; Golder Associates, 1998; EPA, 1996

Table A-11. Maximum Emissions for Other Regulated PSD Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Natural Gas, 50% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	3,390	3,390	3,390
2,3,7,8-TCDD Equivalents (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a) , lb/10 ¹² Btu	1.20E-06	1.20E-06	1.20E-06
Heat Input Rate (MMBtu/hr)	1.21E+03	1.15E+03	1.06E+03
Emission Rate (lb/hr)	1.46E-09	1.38E-09	1.28E-09
(TPY)	2.47E-09	2.33E-09	2.16E-09
Beryllium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a) , lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,214	1,148	1,063
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Fluoride (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (b) , lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,214	1,148	1,063
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Mercury (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a) , lb/10 ¹² Btu	7.48E-04	7.48E-04	7.48E-04
Heat Input Rate (MMBtu/hr)	1,214	1,148	1,063
Emission Rate (lb/hr)	9.08E-07	8.59E-07	7.95E-07
(TPY)	1.54E-06	1.46E-06	1.35E-06
Sulfuric Acid Mist = Fuel Use (lb/hr) x sulfur (S) content (fraction) x conversion of S to H ₂ SO ₄ (%) x MW H ₂ SO ₄ / MW S (98/32)			
Fuel Usage (cf/hr)	1,177,217	1,112,653	1,030,872
Sulfur (lb/hr)	1.68	1.59	1.47
lb H ₂ SO ₄ / lb S (98/32)	3.0625	3.0625	3.0625
Conversion to H ₂ SO ₄ (%) (c)	10	10	10
Emission Rate (lb/hr)	0.52	0.49	0.45
(TPY)	0.87	0.83	0.76

Sources: (a) Golder Associates, 1998; (b) EPA, 1981; (c) Assumed.

Table A-12. Maximum Emissions for Hazardous Air Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Natural Gas, 50% Load

Parameter	Ambient Temperature		95 °F
	32 °F	59 °F	
Hours of Operation	3,390	3,390	3,390
Antimony (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0.00E+00	0.00E+00	0.00E+00
Heat Input Rate (MMBtu/hr)	1,214	1,148	1,063
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Benzene (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0.8	0.8	0.8
Heat Input Rate (MMBtu/hr)	1,214	1,148	1,063
Emission Rate (lb/hr)	9.71E-04	9.18E-04	8.51E-04
(TPY)	1.65E-03	1.56E-03	1.44E-03
Cadmium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,214	1,148	1,063
Emission Rate (lb/hr)	0	0	0
(TPY)	0.00E+00	0.00E+00	0.00E+00
Chromium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,214	1,148	1,063
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Formaldehyde (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	34	34	34
Heat Input Rate (MMBtu/hr)	1,214	1,148	1,063
Emission Rate (lb/hr)	4.13E-02	3.90E-02	3.62E-02
(TPY)	7.00E-02	6.61E-02	6.13E-02
Cobalt (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1.21E+03	1.15E+03	1.06E+03
Emission Rate (lb/hr)	0.00E+00	0.00E+00	0.00E+00
(TPY)	0	0	0
Manganese (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,214	1,148	1,063
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Nickel (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,214	1,148	1,063
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Phosphorous (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (b), lb/10 ¹² Btu	0.00E+00	0.00E+00	0.00E+00
Heat Input Rate (MMBtu/hr)	1,214	1,148	1,063
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Selenium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	0	0	0
Heat Input Rate (MMBtu/hr)	1,214	1,148	1,063
Emission Rate (lb/hr)	0	0	0
(TPY)	0	0	0
Toluene (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	10	10	10
Heat Input Rate (MMBtu/hr)	1,214	1,148	1,063
Emission Rate (lb/hr)	1.21E-02	1.15E-02	1.06E-02
(TPY)	2.06E-02	1.95E-02	1.80E-02

Sources: (a) Colder Associates, 1998; (b) EPA, 1996 (AP-42, Table 3.1-4)

Table A-13. Design Information and Stack Parameters for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Distillate Oil, Base Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Combustion Turbine Performance			
Net power output (MW)	183.9	181.9	171.2
Net heat rate (Btu/kWh, LHV)	10,103	9,929	9,988
(Btu/kWh, HHV)	10,710	10,524	10,588
Heat Input (MMBtu/hr, LHV)	1,858	1,806	1,710
(MMBtu/hr, HHV)	1,969	1,914	1,813
Fuel heating value (Btu/lb, LHV)	18,300	18,300	18,300
(Btu/lb, HHV)	19,398	19,398	19,398
(HHV/LHV)	1.060	1.060	1.060
CT Exhaust Flow			
Mass Flow (lb/hr)- with margin of 10% -	4,230,600	4,081,000	3,825,800
- provided	3,846,000	3,710,000	3,478,000
Temperature (°F)	1,076	1,094	1,121
Moisture (% Vol.)	11	11.7	13.3
Oxygen (% Vol.)	11.20	11.04	10.60
Molecular Weight	28.33	28.25	28.06
Fuel Usage			
Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu (Fuel Heat Content, Btu/lb (LHV))			
Heat input (MMBtu/hr, LHV)	1,858	1,806	1,710
Heat content (Btu/lb, LHV)	18,300	18,300	18,300
Fuel usage (lb/hr)- calculated	101,530	98,689	93,443
CT Stack			
Stack height (ft)	60	60	60
Diameter (ft)	22	22	22
Turbine Flow Conditions			
Turbine Flow (acfm) = [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F) + 460°F)] / [Molecular weight x 2116.8] / 60 min/hr			
Mass flow (lb/hr)	4,230,600	4,081,000	3,825,800
Temperature (°F)	1,076	1,094	1,121
Molecular weight	28.33	28.25	28.06
Volume flow (acfm)- calculated	2,790,601	2,731,215	2,622,427
(ft ³ /s)- calculated	46,510	45,520	43,707
Velocity (ft/sec)	122.4	119.7	115.0

Note: Universal gas constant = 1,545 ft-lb(force)/°R; atmospheric pressure = 2,116.8 lb(force)/ft²; 14.7 lb/ft³

Source: GE, 1999; Golder Associates, 1999

Table A-14. Maximum Emissions for Criteria Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Distillate Oil, Base Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	1,000	1,000	1,000
Particulate (lb/hr) = Emission rate (lb/hr) from manufacturer			
Basis (excludes H ₂ SO ₄), lb/hr	17	17	17
Emission rate (lb/hr)- provided	17.0	17.0	17.0
(TPY)	8.5	8.5	8.5
Sulfur Dioxide (lb/hr) = Natural gas (lb/hr) x sulfur content (%/100) x (lb SO ₂ /lb S)			
Fuel Sulfur Content	0.05%	0.05%	0.05%
Fuel use (lb/hr)	101,530	98,689	93,443
lb SO ₂ /lb S (64/32)	2	2	2
Emission rate (lb/hr)	101.5	98.7	93.4
(TPY)	50.77	49.34	46.72
Nitrogen Oxides (lb/hr) = NOx(ppm) x {[20.9 x (1 - Moisture(%)/100)] - Oxygen(%)} x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]			
Basis, ppmvd @15% O ₂	42	42	42
Moisture (%)	11	11.7	13.3
Oxygen (%)	11.2	11.04	10.6
Turbine Flow (acfm)	2,790,601	2,731,215	2,622,427
Turbine Exhaust Temperature (°F)	1,076	1,094	1,121
Emission rate (lb/hr)	362.0	350.8	335.8
(TPY)	181.0	175.4	167.9
Carbon Monoxide (lb/hr) = CO(ppm) x [1 - Moisture(%)/100] x 2116.8 lb/ft ² x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]			
Basis, ppmvd	20	20	20
Moisture (%)	11	11.7	13.3
Turbine Flow (acfm)	2,790,601	2,731,215	2,622,427
Turbine Exhaust Temperature (°F)	1,076	1,094	1,121
Emission rate (lb/hr)	74.4	71.4	66.2
(TPY)	37.2	35.7	33.1
VOCs (lb/hr) = VOC(ppmvw) x 2116.8 lb/ft ² x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]			
Basis, ppmvw	7	7	7
Turbine Flow (acfm)	2,790,601	2,731,215	2,622,427
Turbine Exhaust Temperature (°F)	1,076	1,094	1,121
Emission rate (lb/hr)	16.73	16.18	15.27
(TPY)	8.4	8.1	7.6
Lead (lb/hr)= NA			
Emission Rate Basis (lb/10 ¹² Btu)	10.8	10.8	10.8
Emission rate (lb/hr)	0.0213	0.0207	0.0196
(TPY)	0.0106	0.0103	0.0098

Note: ppmvd= parts per million, volume dry; O₂= oxygen.

Source: GE, 1998; Golder Associates, 1998; EPA, 1996 (AP-42 draft revisions)

Table A-15. Maximum Emissions for Other Regulated PSD Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Distillate Oil, Base Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	1,000	1,000	1,000
$2,3,7,8 \text{ TCDD Equivalents (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a), lb/10 ¹² Btu	3.38E-04	3.38E-04	3.38E-04
Heat Input Rate (MMBtu/hr)	1.97E+03	1.91E+03	1.81E+03
Emission Rate (lb/hr)	6.66E-07	6.47E-07	6.13E-07
(TPY)	3.33E-07	3.24E-07	3.06E-07
$\text{Beryllium (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a), lb/10 ¹² Btu	0.331	0.331	0.331
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	6.52E-04	6.34E-04	6.00E-04
(TPY)	3.26E-04	3.17E-04	3.00E-04
$\text{Fluoride (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (b), lb/10 ¹² Btu	32.54	32.54	32.54
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	6.41E-02	6.23E-02	5.90E-02
(TPY)	3.20E-02	3.11E-02	2.95E-02
$\text{Hydrogen Chloride (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (c), lb/10 ¹² Btu	2.12E+02	2.12E+02	2.12E+02
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	4.18E-01	4.06E-01	3.84E-01
(TPY)	2.09E-01	2.03E-01	1.92E-01
$\text{Mercury (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a), lb/10 ¹² Btu	6.26E-01	6.26E-01	6.26E-01
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	1.23E-03	1.20E-03	1.13E-03
(TPY)	6.16E-04	5.99E-04	5.67E-04
$\text{Sulfuric Acid Mist} = \text{Fuel Use (lb/hr)} \times \text{sulfur (S) content (fraction)} \times \text{conversion of S to H}_2\text{SO}_4 \text{ (\%)} \\ \times \text{MW H}_2\text{SO}_4 / \text{MW S (98/32)}$			
Fuel Usage (cf/hr)	101,530	98,689	93,443
Sulfur (lb/hr)	50.77	49.34	46.72
lb H ₂ SO ₄ / lb S (98/32)	3.0625	3.0625	3.0625
Conversion to H ₂ SO ₄ (%) (d)	10	10	10
Emission Rate (lb/hr)	15.55	15.11	14.31
(TPY)	7.77	7.56	7.15

Sources: (a) EPA, 1998 (AP-42 draft revisions); (b) EPA, 1981; (c) 4 ppm assumed based on ASTM D2880
(d) assumed based on combustion and HRSG effects.

Table A-16. Maximum Emissions for Hazardous Air Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Distillate Oil, Base Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	1,000	1,000	1,000
Arsenic (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a) , lb/10 ¹² Btu	7.91E+00	7.91E+00	7.91E+00
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	1.56E-02	1.51E-02	1.43E-02
(TPY)	7.79E-03	7.57E-03	7.17E-03
Benzene (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a) , lb/10 ¹² Btu	1.1	1.1	1.1
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	2.17E-03	2.11E-03	1.99E-03
(TPY)	1.08E-03	1.05E-03	9.97E-04
Cadmium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a) , lb/10 ¹² Btu	3.24	3.24	3.24
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	6.38E-03	6.20E-03	5.87E-03
(TPY)	3.19E-03	3.10E-03	2.94E-03
Chromium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a) , lb/10 ¹² Btu	6.76	6.76	6.76
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	1.33E-02	1.29E-02	1.23E-02
(TPY)	6.66E-03	6.47E-03	6.13E-03
Formaldehyde (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a) , lb/10 ¹² Btu	2	2	2
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	3.94E-03	3.83E-03	3.63E-03
(TPY)	1.97E-03	1.91E-03	1.81E-03
Cobalt (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (b) , lb/10 ¹² Btu	37	37	37
Heat Input Rate (MMBtu/hr)	1.97E+03	1.91E+03	1.81E+03
Emission Rate (lb/hr)	7.29E-02	7.08E-02	6.71E-02
(TPY)	3.64E-02	3.54E-02	3.35E-02

Table A-16. Maximum Emissions for Hazardous Air Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Distillate Oil, Base Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
<hr/>			
Manganese (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a) , lb/10 ¹² Btu	432	432	432
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	8.51E-01	8.27E-01	7.83E-01
(TPY)	4.25E-01	4.14E-01	3.92E-01
Nickel (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a) , lb/10 ¹² Btu	86.3	86.3	86.3
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	1.70E-01	1.65E-01	1.56E-01
(TPY)	8.50E-02	8.26E-02	7.82E-02
Phosphorous (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (b) , lb/10 ¹² Btu	3.00E+02	3.00E+02	3.00E+02
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	0.590844	0.574308	0.54378
(TPY)	0.295422	0.287154	0.27189
Selenium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a) , lb/10 ¹² Btu	23	23	23
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	4.53E-02	4.40E-02	4.17E-02
(TPY)	2.26E-02	2.20E-02	2.08E-02
Toluene (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a) , lb/10 ¹² Btu	237	237	237
Heat Input Rate (MMBtu/hr)	1,969	1,914	1,813
Emission Rate (lb/hr)	4.67E-01	4.54E-01	4.30E-01
(TPY)	2.33E-01	2.27E-01	2.15E-01

Sources: (a) EPA, 1998 (AP-42 draft revisions); (b) EPA, 1996 (AP-42, Table 3.1-4)

Table A-17. Design Information and Stack Parameters for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Distillate Oil, 75% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Combustion Turbine Performance			
Net power output (MW)	136.6	132.3	118.5
Net heat rate (Btu/kWh, LHV)	11,069	11,073	11,553
(Btu/kWh, HHV)	11,733	11,738	12,246
Heat Input (MMBtu/hr, LHV)	1,512	1,465	1,369
(MMBtu/hr, HHV)	1,603	1,553	1,451
Fuel heating value (Btu/lb, LHV)	18,300	18,300	18,300
(Btu/lb, HHV)	19,398	19,398	19,398
(HHV/LHV)	1.060	1.060	1.060
CT Exhaust Flow			
Mass Flow (lb/hr)- with margin of 10%	3,287,900	3,225,200	3,106,400
- provided	2,989,000	2,932,000	2,824,000
Temperature (°F)	1,170	1,176	1,186
Moisture (% Vol.)	11.5	11.8	12.9
Oxygen (% Vol.)	10.70	10.80	10.80
Molecular Weight	28.29	28.26	28.12
Fuel Usage			
Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu (Fuel Heat Content, Btu/lb (LHV))			
Heat input (MMBtu/hr, LHV)	1,512	1,465	1,369
Heat content (Btu/lb, LHV)	18,300	18,300	18,300
Fuel usage (lb/hr)- calculated	82,623	80,055	74,809
CT Stack			
CT - Stack height (ft)	60	60	60
Diameter (ft)	22	22	22
Turbine Flow Conditions			
Turbine Flow (acfm) = [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F) + 460°F)] / [Molecular weight x 2116.8] / 60 min/hr			
Mass flow (lb/hr)	3,287,900	3,225,200	3,106,400
Temperature (°F)	1,170	1,176	1,186
Molecular weight	28.29	28.26	28.12
Volume flow (acfm)- calculated	2,304,584	2,271,141	2,212,060
(ft ³ /s)- calculated	38,410	37,852	36,868
Velocity (ft/sec)	101.0	99.6	97.0

Note: Universal gas constant = 1,545 ft-lb(force)/°R; atmospheric pressure = 2,116.8 lb(force)/ft²; 14.7 lb/ft³

Source: GE, 1999; Golder Associates, 1999

Table A-18. Maximum Emissions for Criteria Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Distillate Oil, 75% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	1,000	1,000	1,000
Particulate (lb/hr) = Emission rate (lb/hr) from manufacturer			
Basis (excludes H ₂ SO ₄), lb/hr	17	17	17
Emission rate (lb/hr)- provided	17.0	17.0	17.0
(TPY)	8.5	8.5	8.5
Sulfur Dioxide (lb/hr) = Natural gas (lb/hr) x sulfur content (%/100) x (lb SO ₂ /lb S)			
Fuel Sulfur Content	0.05%	0.05%	0.05%
Fuel use (lb/hr)	82,623	80,055	74,809
lb SO ₂ /lb S (64/32)	2	2	2
Emission rate (lb/hr)	82.6	80.1	74.8
(TPY)	41.31	40.03	37.40
Nitrogen Oxides (lb/hr) = NOx(ppm) x {[20.9 x (1 - Moisture(%)/100)] - Oxygen(%)} x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]			
Basis, ppmvd @15% O ₂	42	42	42
Moisture (%)	11.5	11.8	12.9
Oxygen (%)	10.7	10.8	10.8
Turbine Flow (acfm)	2,304,584	2,271,141	2,212,060
Turbine Exhaust Temperature (°F)	1,170	1,176	1,186
Emission rate (lb/hr)	296.7	285.3	267.8
(TPY)	148.4	142.6	133.9
Carbon Monoxide (lb/hr) = CO(ppm) x [1 - Moisture(%)/100] x 2116.8 lb/ft ² x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]			
Basis, ppmvd	20	20	20
Moisture (%)	11.5	11.8	12.9
Turbine Flow (acfm)	2,304,584	2,271,141	2,212,060
Turbine Exhaust Temperature (°F)	1,170	1,176	1,186
Emission rate (lb/hr)	57.6	56.4	53.9
(TPY)	28.8	28.2	26.9
VOCs (lb/hr) = VOC(ppmvw) x 2116.8 lb/ft ² x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]			
Basis, ppmvw	7	7	7
Turbine Flow (acfm)	2,304,584	2,271,141	2,212,060
Turbine Exhaust Temperature (°F)	1,170	1,176	1,186
Emission rate (lb/hr)	13.02	12.78	12.37
(TPY)	6.5	6.4	6.2
Lead (lb/hr)= NA			
Emission Rate Basis (lb/10 ¹² Btu)	10.8	10.8	10.8
Emission rate (lb/hr)	0.0173	0.0168	0.0157
(TPY)	0.0087	0.0084	0.0078

Note: ppmvd = parts per million, volume dry; O₂ = oxygen.

Source: GE, 1998; Golder Associates, 1998; EPA, 1996 (AP-42 draft revisions)

Table A-19. Maximum Emissions for Other Regulated PSD Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Distillate Oil, 75% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	1,000	1,000	1,000
$2,3,7,8 \text{ TCDD Equivalents (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a) , lb/10 ¹² Btu	3.80E-04	3.80E-04	3.80E-04
Heat Input Rate (MMBtu/hr)	1.60E+03	1.55E+03	1.45E+03
Emission Rate (lb/hr)	6.09E-07	5.90E-07	5.51E-07
(TPY)	3.05E-07	2.95E-07	2.76E-07
$\text{Beryllium (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a) , lb/10 ¹² Btu	0.331	0.331	0.331
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	5.31E-04	5.14E-04	4.80E-04
(TPY)	2.65E-04	2.57E-04	2.40E-04
$\text{Fluoride (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (b) , lb/10 ¹² Btu	32.54	32.54	32.54
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	5.22E-02	5.05E-02	4.72E-02
(TPY)	2.61E-02	2.53E-02	2.36E-02
$\text{Hydrogen Chloride (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (c) , lb/10 ¹² Btu	2.12E+02	2.12E+02	2.12E+02
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	3.40E-01	3.29E-01	3.08E-01
(TPY)	1.70E-01	1.65E-01	1.54E-01
$\text{Mercury (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a) , lb/10 ¹² Btu	6.26E-01	6.26E-01	6.26E-01
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	1.00E-03	9.72E-04	9.08E-04
(TPY)	5.02E-04	4.86E-04	4.54E-04
$\text{Sulfuric Acid Mist} = \text{Fuel Use (lb/hr)} \times \text{sulfur (S) content (fraction)} \times \text{conversion of S to H}_2\text{SO}_4 \text{ (\%)} \\ \times \text{MW H}_2\text{SO}_4 / \text{MW S (98/32)}$			
Fuel Usage (cf/hr)	82,623	80,055	74,809
Sulfur (lb/hr)	41.31	40.03	37.40
lb H ₂ SO ₄ /lb S (98/32)	3.0625	3.0625	3.0625
Conversion to H ₂ SO ₄ (%) (d)	10	10	10
Emission Rate (lb/hr)	12.65	12.26	11.46
(TPY)	6.33	6.13	5.73

Sources: (a) EPA, 1998 (AP-42 draft revisions); (b) EPA, 1981; (c) 4 ppm assumed based on ASTM D2880
(d) assumed based on combustion and HRSG effects.

Table A-20. Maximum Emissions for Hazardous Air Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Distillate Oil, 75% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	1,000	1,000	1,000
Arsenic (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	7.91E+00	7.91E+00	7.91E+00
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	1.27E-02	1.23E-02	1.15E-02
(TPY)	6.34E-03	6.14E-03	5.74E-03
Benzene (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	1.1	1.1	1.1
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	1.76E-03	1.71E-03	1.60E-03
(TPY)	8.81E-04	8.54E-04	7.98E-04
Cadmium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	3.24	3.24	3.24
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	5.19E-03	5.03E-03	4.70E-03
(TPY)	2.60E-03	2.52E-03	2.35E-03
Chromium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	6.76	6.76	6.76
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	1.08E-02	1.05E-02	9.81E-03
(TPY)	5.42E-03	5.25E-03	4.90E-03
Formaldehyde (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	2	2	2
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	3.21E-03	3.11E-03	2.90E-03
(TPY)	1.60E-03	1.55E-03	1.45E-03
Cobalt (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (b), lb/10 ¹² Btu	37	37	37
Heat Input Rate (MMBtu/hr)	1.60E+03	1.55E+03	1.45E+03
Emission Rate (lb/hr)	5.93E-02	5.75E-02	5.37E-02
(TPY)	2.97E-02	2.87E-02	2.68E-02
Manganese (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	432	432	432
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	6.92E-01	6.71E-01	6.27E-01
(TPY)	3.46E-01	3.35E-01	3.13E-01
Nickel (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	86.3	86.3	86.3
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	1.38E-01	1.34E-01	1.25E-01
(TPY)	6.92E-02	6.70E-02	6.26E-02
Phosphorous (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (b), lb/10 ¹² Btu	3.00E+02	3.00E+02	3.00E+02
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	0.480816	0.46587	0.435342
(TPY)	0.240408	0.232935	0.217671
Selenium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	23	23	23
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	3.69E-02	3.57E-02	3.34E-02
(TPY)	1.84E-02	1.79E-02	1.67E-02
Toluene (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	237	237	237
Heat Input Rate (MMBtu/hr)	1,603	1,553	1,451
Emission Rate (lb/hr)	3.80E-01	3.68E-01	3.44E-01
(TPY)	1.90E-01	1.84E-01	1.72E-01

Sources: (a) EPA, 1998 (AP-42 draft revisions); (b) EPA, 1996 (AP-42, Table 3.1-4)

Table A-21. Design Information and Stack Parameters for FPL Sanford Repowering Project
GE Frame 7FA, Dry Low NOx Combustor, Distillate Oil, 50% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Combustion Turbine Performance			
Net power output (MW)	90.2	87.3	77.6
Net heat rate (Btu/kWh, LHV)	13,304	13,162	13,892
(Btu/kWh, HHV)	14,102	13,951	14,725
Heat Input (MMBtu/hr, LHV)	1,200	1,149	1,078
(MMBtu/hr, HHV)	1,272	1,218	1,143
Fuel heating value (Btu/lb, LHV)	18,300	18,300	18,300
(Btu/lb, HHV)	19,398	19,398	19,398
(HHV/LHV)	1.060	1.060	1.060
CT Exhaust Flow			
Mass Flow (lb/hr)- with margin of 10%	2,737,900	2,655,400	2,586,100
- provided	2,489,000	2,414,000	2,351,000
Temperature (°F)	1,200	1,200	1,200
Moisture (% Vol.)	11.2	11.6	12.7
Oxygen (% Vol.)	11.10	11.20	11.30
Molecular Weight	28.29	28.24	28.10
Fuel Usage			
Fuel usage (lb/hr) = Heat Input (MMBtu/hr) x 1,000,000 Btu/MMBtu (Fuel Heat Content, Btu/lb (LHV))			
Heat input (MMBtu/hr, LHV)	1,200	1,149	1,078
Heat content (Btu/lb, LHV)	18,300	18,300	18,300
Fuel usage (lb/hr)- calculated	65,574	62,787	58,907
CT Stack			
CT - Stack height (ft)	60	60	60
Diameter (ft)	22	22	22
Turbine Flow Conditions			
Turbine Flow (acfm) = [(Mass Flow (lb/hr) x 1,545 x (Temp. (°F) + 460°F)] / [Molecular weight x 2116.8] / 60 min/hr			
Mass flow (lb/hr)	2,737,900	2,655,400	2,586,100
Temperature (°F)	1,200	1,200	1,200
Molecular weight	28.29	28.24	28.10
Volume flow (acfm)- calculated	1,954,205	1,898,809	1,858,599
(ft ³ /s)- calculated	32,570	31,647	30,977
Velocity (ft/sec)	85.7	83.3	81.5

Note: Universal gas constant = 1,545 ft-lb(force)/°R; atmospheric pressure = 2,116.8 lb(force)/ft²; 14.7 lb/ft³

Source: GE, 1999; Golder Associates, 1999

Table A-22. Maximum Emissions for Criteria Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Distillate Oil, 50% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	1,000	1,000	1,000
Particulate (lb/hr) = Emission rate (lb/hr) from manufacturer			
Basis (excludes H ₂ SO ₄), lb/hr	17	17	17
Emission rate (lb/hr)- provided	17.0	17.0	17.0
(TPY)	8.5	8.5	8.5
Sulfur Dioxide (lb/hr) = Natural gas (lb/hr) x sulfur content (%/100) x (lb SO ₂ /lb S)			
Fuel Sulfur Content	0.05%	0.05%	0.05%
Fuel use (lb/hr)	65,574	62,787	58,907
lb SO ₂ /lb S (64/32)	2	2	2
Emission rate (lb/hr)	65.6	62.8	58.9
(TPY)	32.79	31.39	29.45
Nitrogen Oxides (lb/hr) = NOx(ppm) x {[20.9 x (1 - Moisture(%)/100)] - Oxygen(%)} x 2116.8 x Volume flow (acfm) x 46 (mole. wgt NOx) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 5.9 x 1,000,000 (adj. for ppm)]			
Basis, ppmvd @15% O ₂	42	42	42
Moisture (%)	11.2	11.6	12.7
Oxygen (%)	11.1	11.2	11.3
Turbine Flow (acfm)	1,954,205	1,898,809	1,858,599
Turbine Exhaust Temperature (°F)	1,200	1,200	1,200
Emission rate (lb/hr)	236.4	224.0	209.3
(TPY)	118.2	112.0	104.7
Carbon Monoxide (lb/hr) = CO(ppm) x [1 - Moisture(%)/100] x 2116.8 lb/ft ² x Volume flow (acfm) x 28 (mole. wgt CO) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]			
Basis, ppmvd	30	30	30
Moisture (%)	11.2	11.6	12.7
Turbine Flow (acfm)	1,954,205	1,898,809	1,858,599
Turbine Exhaust Temperature (°F)	1,200	1,200	1,200
Emission rate (lb/hr)	72.2	69.8	67.5
(TPY)	36.1	34.9	33.7
VOCs (lb/hr) = VOC(ppmvw) x 2116.8 lb/ft ² x Volume flow (acfm) x 16 (mole. wgt as methane) x 60 min/hr / [1545 x (CT temp.(°F) + 460°F) x 1,000,000 (adj. for ppm)]			
Basis, ppmvw	7	7	7
Turbine Flow (acfm)	1,954,205	1,898,809	1,858,599
Turbine Exhaust Temperature (°F)	1,200	1,200	1,200
Emission rate (lb/hr)	10.84	10.53	10.31
(TPY)	5.4	5.3	5.2
Lead (lb/hr)= NA			
Emission Rate Basis (lb/10 ¹² Btu)	10.8	10.8	10.8
Emission rate (lb/hr)	0.0137	0.0132	0.0123
(TPY)	0.0069	0.0066	0.0062

Note: ppmvd= parts per million, volume dry; O₂= oxygen.

Source: GE, 1998; Golder Associates, 1998; EPA, 1996 (AP-42 draft revisions)

Table A-23. Maximum Emissions for Other Regulated PSD Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Distillate Oil, 50% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	1,000	1,000	1,000
$2,3,7,8 \text{ TCDD Equivalents (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a) , lb/10 ¹² Btu	3.80E-04	3.80E-04	3.80E-04
Heat Input Rate (MMBtu/hr)	1.27E+03	1.22E+03	1.14E+03
Emission Rate (lb/hr)	4.83E-07	4.63E-07	4.34E-07
(TPY)	2.42E-07	2.31E-07	2.17E-07
$\text{Beryllium (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a) , lb/10 ¹² Btu	0.331	0.331	0.331
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	4.21E-04	4.03E-04	3.78E-04
(TPY)	2.11E-04	2.02E-04	1.89E-04
$\text{Fluoride (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (b) , lb/10 ¹² Btu	32.54	32.54	32.54
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	4.14E-02	3.96E-02	3.72E-02
(TPY)	2.07E-02	1.98E-02	1.86E-02
$\text{Hydrogen Chloride (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (c) , lb/10 ¹² Btu	2.12E+02	2.12E+02	2.12E+02
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	2.70E-01	2.58E-01	2.42E-01
(TPY)	1.35E-01	1.29E-01	1.21E-01
$\text{Mercury (lb/hr)} = \text{Basis (lb/10}^{12} \text{ Btu)} \times \text{Heat Input (MMBtu/hr)} / 1,000,000 \text{ MMBtu/10}^{12} \text{ Btu}$			
Basis (a) , lb/10 ¹² Btu	6.26E-01	6.26E-01	6.26E-01
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	7.96E-04	7.62E-04	7.15E-04
(TPY)	3.98E-04	3.81E-04	3.58E-04
$\text{Sulfuric Acid Mist} = \text{Fuel Use (lb/hr)} \times \text{sulfur (S) content (fraction)} \times \text{conversion of S to H}_2\text{SO}_4 \text{ (\%)} \\ \times \text{MW H}_2\text{SO}_4 / \text{MW S (98/32)}$			
Fuel Usage (cf/hr)	65,574	62,787	58,907
Sulfur (lb/hr)	32.79	31.39	29.45
lb H ₂ SO ₄ /lb S (98/32)	3.0625	3.0625	3.0625
Conversion to H ₂ SO ₄ (%) (d)	10	10	10
Emission Rate (lb/hr)	10.04	9.61	9.02
(TPY)	5.02	4.81	4.51

Sources: (a) EPA, 1998 (AP-42 draft revisions); (b) EPA, 1981; (c) 4 ppm assumed based on ASTM D2880
(d) assumed based on combustion and HRSG effects.

Table A-24. Maximum Emissions for Hazardous Air Pollutants for IPS - Vandolah
GE Frame 7FA, Dry Low NOx Combustor, Distillate Oil, 50% Load

Parameter	Ambient Temperature		
	32 °F	59 °F	95 °F
Hours of Operation	1,000	1,000	1,000
Arsenic (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	7.91E+00	7.91E+00	7.91E+00
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	1.01E-02	9.63E-03	9.04E-03
(TPY)	5.03E-03	4.82E-03	4.52E-03
Benzene (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	1.1	1.1	1.1
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	1.40E-03	1.34E-03	1.26E-03
(TPY)	7.00E-04	6.70E-04	6.28E-04
Cadmium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	3.24	3.24	3.24
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	4.12E-03	3.95E-03	3.70E-03
(TPY)	2.06E-03	1.97E-03	1.85E-03
Chromium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	6.76	6.76	6.76
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	8.60E-03	8.23E-03	7.72E-03
(TPY)	4.30E-03	4.12E-03	3.86E-03
Formaldehyde (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	2	2	2
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	2.54E-03	2.44E-03	2.29E-03
(TPY)	1.27E-03	1.22E-03	1.14E-03
Cobalt (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (b), lb/10 ¹² Btu	37	37	37
Heat Input Rate (MMBtu/hr)	1.27E+03	1.22E+03	1.14E+03
Emission Rate (lb/hr)	4.71E-02	4.51E-02	4.23E-02
(TPY)	2.35E-02	2.25E-02	2.11E-02
Manganese (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	432	432	432
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	5.50E-01	5.26E-01	4.94E-01
(TPY)	2.75E-01	2.63E-01	2.47E-01
Nickel (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	86.3	86.3	86.3
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	1.10E-01	1.05E-01	9.86E-02
(TPY)	5.49E-02	5.26E-02	4.93E-02
Phosphorous (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (b), lb/10 ¹² Btu	3.00E+02	3.00E+02	3.00E+02
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	0.3816	0.365382	0.342804
(TPY)	0.1908	0.182691	0.171402
Selenium (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	23	23	23
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	2.93E-02	2.80E-02	2.63E-02
(TPY)	1.46E-02	1.40E-02	1.31E-02
Toluene (lb/hr) = Basis (lb/10 ¹² Btu) x Heat Input (MMBtu/hr) / 1,000,000 MMBtu/10 ¹² Btu			
Basis (a), lb/10 ¹² Btu	237	237	237
Heat Input Rate (MMBtu/hr)	1,272	1,218	1,143
Emission Rate (lb/hr)	3.01E-01	2.89E-01	2.71E-01
(TPY)	1.51E-01	1.44E-01	1.35E-01

Sources: (a) EPA, 1998 (AP-42 draft revisions); (b) EPA, 1996 (AP-42, Table 3.1-4)

APPENDIX B

**BEST AVAILABLE CONTROL TECHNOLOGY FOR
THE PROPOSED COMBUSTION TURBINES**

B.1 NEW SOURCE PERFORMANCE STANDARDS

The NSPS regulations (40 CFR, Subpart GG) applicable to gas turbines apply to:

1. Electric utility stationary gas turbines with a heat input at peak load of greater than 100×10^6 Btu/hr [40 CFR 60.332 (b)];
2. Stationary gas turbines with a heat input at peak load between 10 and 100×10^6 Btu/hr [40 CFR 60.332 (c)]; or
3. Stationary gas turbines with a manufacturer's rate base load at ISO conditions of 30 MW or less [40 CFR 60.332 (d)].

The electric utility stationary gas turbine provisions apply to stationary gas turbines constructed for the purpose of supplying more than one-third of their potential electric output capacity for sale to any utility power distribution system [40 CFR 60.331 (q)]. The requirements for electric utility stationary gas turbines are applicable to the proposed project and are the most stringent provision of the NSPS. These requirements are summarized in Table B-1 and were considered in the BACT analysis.

As noted from Table B-1, the NSPS NO_x emission limit can be adjusted upward to allow for fuel-bound nitrogen (FBN). For a fuel-bound nitrogen concentration of 0.015 percent or less, no increase in the NSPS is provided; for a fuel-bound nitrogen concentration of 0.03 percent, the NSPS is increased by 0.0012 percent or 12 parts per million (ppm).

B.2 BEST AVAILABLE CONTROL TECHNOLOGY

B.2.1 NITROGEN OXIDES

Advanced dry low- NO_x combustion alone has increasingly been approved by regulatory agencies as BACT and is technically feasible for the proposed project. Available information suggests that SCR with dry low- NO_x combustor technology or with wet injection is also technically feasible. For the "F" Class Project, advanced dry low- NO_x combustor technology is equivalent to the SCR technology and has several important advantages.

B.2.1.1 Identification of NO_x Control Technologies

NO_x emissions from combustion of fossil fuels consist of thermal NO_x and fuel-bound NO_x .

Thermal NO_x is formed from the reaction of oxygen and nitrogen in the combustion air at combustion temperatures. Formation of thermal NO_x depends on the flame temperature, residence time, combustion pressure, and air-to-fuel ratios in the primary combustion zone. The design and

operation of the combustion chamber dictates these conditions. Fuel-bound NO_x is created by the oxidation of volatilized nitrogen in the fuel. Nitrogen content in the fuel is the primary factor in its formation.

Table B-2 presents a listing of the lowest achievable emission rates/best available control technology (LAER/BACT) decisions made by state environmental agencies and EPA regional offices for gas turbines. This table was developed from the information obtained from BACT/LAER Information System (BLIS) database maintained at EPA's National Computer Center located at Research Triangle Park, North Carolina, (e.g., the California Air Control Board, the South Coast Air Quality Management District, the New Jersey Department of Environmental Protection, and the Rhode Island Department of Environmental Management).

Historically, the most stringent NO_x controls for CTs established as LAER/BACT by state agencies were selective catalytic reduction (SCR) with wet injection and wet injection alone. When SCR has been employed, wet injection is used initially to reduce NO_x emissions. However, advanced dry low- NO_x technology has only recently been developed and made available for gas turbines. SCR is a post-combustion control, while advanced dry low- NO_x combustors minimize the formation of NO_x in the combustion process.

SCR has been installed or permitted in over 100 projects. The majority of these projects (more than 90 percent) are cogeneration facilities with capacities of 50 MW or less. About 80 percent of the projects have been in California. Of these 109 projects that have either installed SCR or have been permitted with SCR, about 40 percent have been in the Southern California NO_2 nonattainment area where SCR was required not as BACT but as LAER, a more stringent requirement. LAER is distinctly different from BACT in that there is no consideration of economic, energy, or environmental impacts; if a control technology has previously been installed, it must be required as LAER. LAER is defined as follows:

Lowest achievable emission rate means, for any source, the more stringent rate of emissions based on the following: (i) The most stringent emissions limitation which is contained in the implementation plan of any State of such class or category of stationary source, unless the owner or operator of the proposed stationary source demonstrates that such limitations are not achievable; or (ii) The most stringent emissions limitation which is achieved in practice by such class or category of stationary source. This limitation, when applied to a modification, means the lowest achievable emissions rate for the new or modified emissions units within the stationary source. In no event shall the application of this term permit a proposed new

modified stationary source to emit any pollutant in excess of the amount allowable under applicable new source standards of performance (40 CFR 51, Appendix S.II, A.18).

As noted previously, there are distinct regulatory and policy differences between LAER and BACT. BACT involves an evaluation of the economic, environmental, and energy impacts of alternative control technologies. In contrast, LAER only considers the technical aspects of control.

All the projects in California have natural gas as the primary fuel; only 15 of the SCR applications have distillate fuel as backup. The remaining projects with SCR (i.e., about 25 projects) are located in the eastern United States: Vermont, Massachusetts, Connecticut, New Jersey, New York, Rhode Island, and Virginia. A majority of these projects are cogenerators or independent power producers. The size of these projects ranges from 22 MW to 450 MW, with nearly 90 percent less than 100 MW in size.

Reported and permitted NO_x removal efficiencies of SCR range from 40 to 80 percent of NO_x in the exhaust gas stream. The most common emission limiting standards associated with SCR are approximately 9 ppm for natural gas firing. However, a few facilities have reported emission limits of about 4.5 ppm. These emission limits were clearly determined to be LAER on CTs using water injection with uncontrolled NO_x levels below 42 ppm.

The installation of SCR has primarily been on combined cycle units where the catalyst is located in the HRSG at the proper temperature range. SCR has been installed on two simple cycle projects in California on machines significantly smaller (less than 25 MW) than the "F" Class proposed. With smaller turbines, the exhaust as temperature is lower making possible the installation of high temperature catalysts. Exhaust temperatures from the "F" Class CTs will approach 1,200°F and monitoring and control systems will be required to prevent catalyst damage. The high temperature catalyst are more than 2 times more costly than conventional base metal catalysts that are installed in HRSG. While manufacturers guarantee the high temperature catalysts for 3 years, operating experience at temperatures above 1,000°F is limited. Continuous exposure at these elevated temperatures suggest a more limited life of the SCR system.

Wet injection historically has been the primary method of reducing NO_x emissions from CTs. Indeed, this method of control was first mandated by the NSPS to reduce NO_x levels to 75 parts per million by volume, dry (ppmvd) (corrected to 15 percent O₂ and heat rate). Development of improved wet injection combustors reduced NO_x concentrations to 25 ppmvd (corrected to

15 percent O₂) when burning natural gas. More recently, however, CT manufacturers have developed dry low-NO_x combustors that can reduce NO_x concentrations to 25 ppmvd (corrected to 15 percent O₂) or less when firing natural gas.

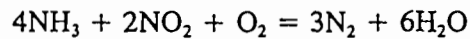
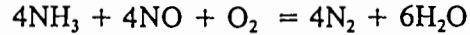
In Florida, all of the most recent PSD permits and BACT determinations for simple cycle gas turbines have required either wet injection or dry low-NO_x technology for NO_x control. The emission limits included in these permits and BACT determinations are primarily in the range of 9 ppmvd to 25 ppmvd (corrected to 15 percent O₂, dry conditions) for future operations on natural-gas firing.

B.2.1.2 Technology Description and Feasibility

Wet Injection--The injection of water or steam in the combustion zone of CTs reduces the flame temperature with a corresponding decrease of NO_x emissions. The amount of NO_x reduction possible depends on the combustor design and the water-to-fuel ratio employed. An increase in the water-to-fuel ratio will cause a concomitant decrease in NO_x emissions until flame instability occurs. At this point, operation of the CT becomes inefficient and unreliable, and significant increases in products of incomplete combustion will occur (i.e., CO and VOC emissions).

Dry Low-NO_x Combustor--In the past several years, CT manufacturers have offered and installed machines with dry low-NO_x combustors. These combustors, which are offered on conventional machines manufactured by Westinghouse, GE, Kraftwerk Union, and ABB, can achieve NO_x concentrations of 25 ppmvd or less when firing natural gas. Westinghouse and GE have offered dry low-NO_x combustors on advanced heavy-duty industrial machines. Thermal NO_x formation is inhibited by using combustion techniques where the natural gas and combustion air are premixed before ignition. For the CT being considered for the project, the combustion chamber design includes the use of dry low-NO_x combustor technology. The NO_x emission level when firing natural gas at baseload conditions is 9 ppmvd (corrected to 9 percent O₂), a level which is available for the project.

Selective Catalytic Reduction (SCR)--SCR uses ammonia (NH₃) to react with NO_x in the gas stream in the presence of a catalyst. NH₃, which is diluted with air to about 5 percent by volume, is introduced into the gas stream at reaction temperatures between 600°F and 750°F. The reactions are as follows:



SCR operating experience, as applied to gas turbines, consists primarily of baseload natural-gas-fired installations either of cogeneration or combined cycle configuration; no simple cycle facilities have SCR. Exhaust gas temperatures of simple cycle CTs generally are in the range of 1,000°F, which exceeds the optimum range for SCR with base metal catalysts. All current SCR applications have the catalyst placed in the HRSG to achieve proper reaction conditions. This allows a relatively constant temperature for the reaction of NH_3 and NO_x on the catalyst surface.

The use of SCR has been limited to facilities that burn natural gas or small amounts of fuel oil since SCR catalysts are contaminated by sulfur-containing fuels (i.e., fuel oil). For most fuel-oil-burning facilities, catalyst operation is discontinued, or the exhaust bypasses the SCR system. While the operating experience with SCR has not been extensive, certain cost, technical, and environmental considerations have surfaced for units firing both natural gas and oil while using SCR.

Ammonium salts (ammonium sulfate and bisulfate) are formed by the reaction of NH_3 and sulfur combustion products. Ammonium bisulfate can be corrosive and could cause damage to the surfaces that follow the catalyst, as well as to the stack. Corrosion protection for these areas would be required with concomitant cost and technical requirements. Ammonium sulfate is emitted as particulate matter. While the formation of ammonium salts is primarily associated with oil firing, sulfur combustion products from natural gas also could form small amounts of ammonium salts.

Zeolite and specially designed high temperature catalysts, which are reported to be capable of operating in temperature ranges up to 1,050°F, have become available commercially only recently. Their application with SCR primarily has been limited to internal combustion engines. Optimum performance of an SCR system using a zeolite catalyst is reported to range from about 800°F to 900°F. At temperatures of 1,050°F and above, the high-temperature catalyst will be irreparably damaged. Application of an SCR system using a zeolite catalyst would be feasible for the project; however, use in simple cycle operation will require monitoring to assure the temperature limits are not exceeded. If temperatures are exceeded then exhaust gas cooling would be required.

increase in fuel consumption, an increase in the volume of gases that must be treated by the control system, and an increase in uncontrolled air emissions, including NO_x.

Thermal DeNO_x--Thermal DeNO_x is Exxon Research and Engineering Company's patented process for NO_x reduction. The process is a high temperature selective noncatalytic reduction (SNCR) of NO_x using ammonia as the reducing agent. Thermal DeNO_x requires the exhaust gas temperature to be above 1,800°F. However, use of ammonia plus hydrogen lowers the temperature requirement to about 1,000°F. For some applications, this must be achieved by additional firing in the exhaust stream before ammonia injection.

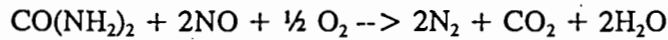
The only known commercial applications of Thermal DeNO_x are on heavy industrial boilers, large furnaces, and incinerators that consistently produce exhaust gas temperatures above 1,800°F. There are no known applications on or experience with CTs. Temperatures of 1,800°F require alloy materials constructed with very large piping and components since the exhaust gas volume would be increased by several times. As with the NO_xOUT process, high capital, operating, and maintenance costs are expected because of material requirements, an additional duct burner system, and fuel consumption. Uncontrolled emissions would increase because of the additional fuel burning.

Thus, the Thermal DeNO_x process will not be considered for the proposed project since its high application temperature makes it technically infeasible. The maximum exhaust gas temperature of a combustion turbine is typically about 1,000°F; the cost to raise the exhaust gas to such a high temperature is prohibitively expensive.

Nonselective Catalytic Reduction--Certain manufacturers, such as Engelhard, market a nonselective catalytic reduction system (NSCR) for NO_x control on reciprocating engines. The NSCR process requires a low oxygen content in the exhaust gas stream and high temperature (700°F to 1,400°F) in order to be effective. CTs have the required temperature but also have high oxygen levels (greater than 12 percent) and, therefore, cannot use the NSCR process. As a result, NSCR is not a technically feasible add-on NO_x control device for CTs.

Technology Determination--A technical evaluation of available post-combustion gas controls (i.e., NO_xOUT, Thermal DeNO_x, and NSCR) indicates that these processes have not been applied to

NO_xOUT Process--The NO_xOUT process originated from the initial research by the Electric Power Research Institute (EPRI) in 1976 on the use of urea to reduce NO_x. EPRI licensed the proprietary process to Fuel Tech, Inc., for commercialization. In the NO_xOUT process, aqueous urea is injected into the flue gas stream ideally within a temperature range of 1,600°F to 1,900°F. In the presence of oxygen, the following reaction results:



The amount of urea required is most cost-effective when the treatment rate is 0.5 to 2 moles of urea per mole of NO_x. In addition to the original EPRI urea patents, Fuel Tech claims to have a number of proprietary catalysts capable of expanding the effective temperature range of the reaction to between 1,600°F and 1,950°F. Advantages of the system are as follows:

1. Low capital and operating costs as a result of use of urea injection, and
2. The proprietary catalysts used are nontoxic and nonhazardous, thus eliminating potential disposal problems.

Disadvantages of the system are as follows:

1. Formation of ammonia from excess urea treatment rates and/or improper use of reagent catalysts, and
2. Sulfur trioxide (SO₃), if present, will react with ammonia created from the urea to form ammonium bisulfate, potentially plugging the cold end equipment downstream.

Commercial application of the NO_xOUT system is limited to three reported cases:

1. Trial demonstration on a 62.5-ton-per-hour (TPH) stoker-fired wood waste boiler with 60 to 65 percent NO_x reduction,
2. A 600 x 10⁶ Btu CO boiler with 60 to 70 percent NO_x reduction, and
3. A 75-MW pulverized coal-fired unit with 65 percent NO_x reduction.

The NO_xOUT system has not been demonstrated on any combustion turbine/HRSG unit.

The NO_xOUT process is not technically feasible for the proposed project because of the high application temperature of 1,600°F to 1,950°F. The maximum exhaust gas temperature of the "F" Class CT is about 1,150°F. Raising the exhaust temperature the required amount essentially would require installation of a heater. This would be economically prohibitive and would result in an

CT/HRSG and are technically infeasible for the project because of process constraints (e.g., temperature).

For the BACT analysis, dry low-NO_x combustion technology is technically feasible and SCR in combination with combustion controls is a potentially feasible alternative that can achieve a maximum degree of emission reduction. The advanced dry low-NO_x combustor alone can achieve 9 ppm (corrected) and the SCR with dry low-NO_x combustor is capable of achieving a NO_x emission level of 3.6 ppm when firing natural gas (corrected to 15 percent O₂ dry conditions). When firing oil, the emissions with SCR and wet injection would be about 16.8 ppm (corrected), whereas emissions with wet injection alone would be 42 ppm (corrected). The SCR has a NO_x removal rate of 60 percent based on an associated ammonia slip (i.e., to 10 ppm).

B.2.1.3 SCR Cost Estimates

Tables B-3 and B-4 present the total capital and annualized cost for SCR, respectively. The costs were developed using EPA Cost Control Manual (EPA, 1990 and 1993). The cost for the SCR system was based on vendor estimates. Standard EPA recommended cost factors were used. For simple cycle operation, a capital recovery period of 15 years was used. However, the SCR system would be subjected to temperatures exceeding 1,000°F where considerable wear can take place resulting in lower life of equipment.

B.2.2 CARBON MONOXIDE

B.2.2.1 Identification of CO Control Technologies

CO emissions are a result of incomplete or partial combustion of fossil fuel. Combustion design and catalytic oxidation are the control alternatives that are viable for the project. Table B-5 presents a listing of LAER/BACT decisions for CO emissions from combustion turbines. Combustion design is the more common control technique used in CTs. Sufficient time, temperature, and turbulence is required within the combustion zone to maximize combustion efficiency and minimize the emissions of CO. Combustion efficiency is dependent upon combustor design. For the CTs being evaluated, CO emissions will not exceed 12 ppmvd, corrected to dry conditions when firing natural gas under full load conditions and 20 ppmvd when firing distillate oil at baseload.

Catalytic oxidation is a post-combustion control that has been employed in CO nonattainment areas where regulations have required CO emission levels to be less than those associated with wet

injection. These installations have been required to use LAER technology and typically have CO limits in the 10 ppm range (corrected to dry conditions).

B.2.2.2 Technology Description

In an oxidation catalyst control system, CO emissions are reduced by allowing unburned CO to react with oxygen at the surface of a precious metal catalyst, such as platinum. Combustion of CO starts at about 300°F, with efficiencies above 90 percent occurring at temperatures above 600°F. Catalytic oxidation occurs at temperatures 50 percent lower than that of thermal oxidation, which reduces the amount of thermal energy required.

For CTs, the oxidation catalyst can be located directly after the CT. Catalyst size depends upon the exhaust flow, temperature, and desired efficiency. The existing oxidation catalyst applications primarily have been limited to smaller cogeneration facilities burning natural gas. Oxidation catalysts have not been used on fuel-oil-fired CTs or combined cycle facilities. The use of sulfur-containing fuels in an oxidation catalyst system would result in an increase of SO₃ emissions and concomitant corrosive effects to the stack. In addition, trace metals in the fuel could result in catalyst poisoning during prolonged periods of operation.

Since the units likely will require numerous startups, variations in exhaust conditions will influence catalyst life and performance. Very little technical data exist to demonstrate the effect of such cycling.

The lack of demonstrated operation with oil firing suggests rejection of catalytic oxidation as a technically feasible alternative. However, the advent of a second generation catalyst suggests that an oxidation catalyst could be used although none have been placed in actual operation.

B.2.2.3 Oxidation Catalyst Costs

Tables B-6 and B-7 present the capital and annualized cost for an oxidation catalyst. The maximum CO impacts are less than 0.1 percent of the applicable ambient air quality standards. There would also be no secondary benefits, such as acidic deposition, to reducing CO.

Table B-1. Federal NSPS for Electric Utility Stationary Gas Turbines

Pollutant	Emission Limitation ^a
Nitrogen Oxides ^b	0.0075 percent by volume (75 ppm) at 15 percent O ₂ on a dry basis adjusted for heat rate and fuel nitrogen

^a Applicable to electric utility gas turbines with a heat input at peak load of greater than 100 x 10⁶ Btu/hr.

^b Standard is multiplied by 14.4/Y; where Y is the manufacturer's rated heat rate in kilojoules per watt at rated load or actual measured heat rate based on the lower heating value of fuel measured at actual peak load; Y cannot be greater than 14.4. Standard is adjusted upward (additive) by the percent of nitrogen in the fuel:

Fuel-Bound Nitrogen (percent by weight)	Allowed Increase NO _x Percent by Volume
$N \leq 0.015$	0
$0.015 < N \leq 0.1$	0.04(N)
$0.1 < N \leq 0.25$	$0.004 + 0.0067(N - 0.1)$
$N > 0.25$	0.005

where: N = the nitrogen content of the fuel (percent by weight).

Source: 40 CFR 60 Subpart GG.

Table B-2. Summary of Best Available Control Technology (BACT) Determinations for Nitrogen Oxide (NOx) Emissions

Facility Name	State	Permit Issue Date	Unit/Process Description	Capacity (size)	NOx Emission Limit	Control Method	Efficiency (%)	Type
SOUTHERN NATURAL GAS	AL	Mar-98	2-9160 HP GE MODEL MS30020 NATURAL GAS TURBINES	9,160 HP	53 LB/HR		0	BACT-PSD
SOUTHERN NATURAL GAS	AL	Mar-98	9160 HP GE MODEL MS30020 NATURAL GAS FIRED TURBINE	9,160 HP	53 LB/HR		0	BACT-PSD
ALABAMA POWER COMPANY	AL	Dec-97	COMBUSTION TURBINE W/ DUCT BURNER (COMBINED CYCL	100 MW	15 PPM	DRY LOW NOX BURNERS	0	BACT-PSD
BUCKNELL UNIVERSITY	PA	Nov-97	NO FIRED TURBINE, SOLAR TAURUS T-7300S	5.0 MW	25 PPMV @ 15% O2	SOLONOX BURNER; LOW NOX BURNER	0	BACT-OTHER
NORTHERN CALIFORNIA POWER AGENCY	CA	Oct-97	GE FRAME 5 GAS TURBINE	325 MMBTU/HR	25 PPMV @ 15% O2	DRY LOW NOX BURNERS	0	LAER
LORDSBURG L.P.	NM	Jun-97	TURBINE, NATURAL GAS-FIRED, ELEC. GEN.	100 MW	74.4 LB/HR	DRY LOW-NOX TECHNOLOGY WHICH ADOPTS STAGED OR SCHEDULED COMBUSTION.	80	BACT-PSD
SOUTHERN CALIFORNIA GAS COMPANY	CA	May-97	VARIABLE LOAD NATURAL GAS FIRED TURBINE COMPRESSOR	50 MMBTU/HR	25 PPMV @ 15% O2	DRY LOW NOX COMBUSTOR FUEL OIL SULFUR CONTENT <= 0.05% BY WEIGHT, DRY LOW NOX COMBUSTOR DESIGN FIRING GAS AND DRY LOW NOX COMBUSTOR	0	LAER
MEAD COATED BOARD, INC.	AL	Mar-97	COMBINED CYCLE TURBINE (25 MW)	568 MMBTU/HR	25 PPMV @ 15% O2 (GAS)	WITH WATER INJECTION FIRING OIL	0	BACT-PSD
FORMOSA PLASTICS CORPORATION, BATON ROUGE PLANT	LA	Mar-97	TURBINE/HSRO, GAS COGENERATION	450 MM BTU/HR	9 PPMV	DRY LOW NOX BURNER/COMBUSTION DESIGN AND	0	BACT-PSD
SOUTHWESTERN PUBLIC SERVICE COMPANY/CUNNINGHAM STA	NM	Feb-97	COMBUSTION TURBINE, NATURAL GAS	100 MW	0 SEE FACILITY NOTES	DRY LOW NOX COMBUSTION	0	BACT-PSD
CALRESOURCES LLC	CA	Jan-97	SOLAR MODEL 1100 SATURN GAS TURBINE	14 MMBTU/HR	69 PPMV @ 15% O2	NO CONTROL	0	LAER
TEMPO PLASTICS	CA	Oct-96	GAS TURBINE COGENERATION UNIT	0.0	0.109 LB/AMBTU	LOW-NOX COMBUSTOR	0	LAER
SOUTHERN NATURAL GAS COMPANY	MS	Dec-96	TURBINE, NATURAL GAS-FIRED	9,160 HORSEPOWER	110 PPMV @ 15% O2, DRY	PROPER TURBINE DESIGN AND OPERATION	0	BACT-PSD
SOUTHERN NATURAL GAS COMPANY-SELMA COMPRESSOR STAT	AL	Dec-96	9160 HP GE MS30020 NATURAL GAS FIRED TURBINE	0.0	53 LB/HR		0	BACT-PSO
SOUTHWESTERN PUBLIC SERVICE CO/CUNNINGHAM STATION	NM	Nov-96	COMBUSTION TURBINE, NATURAL GAS	100 MW	15 PPM; SEE FAC. NOTES	DRY LOW NOX COMBUSTION STEAM/WATER INJECTION AND SELECTIVE CATALYTIC REDUCTION (SCR)	0	BACT-PSD
ECOELECTRICA, L.P.	PR	Oct-96	TURBINES, COMBINED-CYCLE COGENERATION	461 MW	60 LB/HR (GAS)	STEAM/WATER INJECTION AND SELECTIVE CATALYTIC REDUCTION (SCR)	72	BACT-PSD
ECOELECTRICA, L.P.	PR	Oct-96	TURBINES, COMBINED-CYCLE COGENERATION	461 MW	73 LB/HR (OIL)	STEAM/WATER INJECTION AND SELECTIVE CATALYTIC REDUCTION (SCR)	72	BACT-PSD
BLUE MOUNTAIN POWER, LP	PA	Jul-96	COMBUSTION TURBINE WITH HEAT RECOVERY BOILER	153 MW	4 PPM @ 15% O2	DRY LOW NOX COMBUSTOR	0	BACT-PSD
CITY OF ST. PAUL POWER PLANT	AK	Jun-96	INTERNAL COMBUSTION	3.4 MW	427 TPY	AFTERCOOLERS	0	BACT-PSD
CITY OF UNALASKA	AK	Jun-96	INTERNAL COMBUSTION	6.5 MW	633 TPY	LIMIT OF OPERATION HOURS AND AFTERCOOLERS	0	BACT-PSO
GENERAL ELECTRIC GAS TURBINES	SC	Apr-96	I.C. TURBINE	2,700 MMBTU/HR	885 LB/HR	GOOD COMBUSTION PRACTICES TO MINIMIZE EMISSIONS	0	BACT-PSD
CAROLINA POWER & LIGHT	NC	Apr-96	COMBUSTION TURBINE, 4 EACH	1,908 MMBTU/HR	512 LB/HR (OIL)	WATER INJECTION; FUEL SPEC: 0.04% N FUEL OIL	0	BACT-PSD
CAROLINA POWER & LIGHT	NC	Apr-96	COMBUSTION TURBINE, 4 EACH	1,908 MMBTU/HR	158 LB/HR (GAS)	WATER INJECTION	0	BACT-PSD
MID-GEORGIA COGEN.	GA	Apr-96	COMBUSTION TURBINE (2), FUEL OIL	116 MW	20 PPMV	WATER INJECTION WITH SCR	0	BACT-PSD
MID-GEORGIA COGEN.	GA	Apr-96	COMBUSTION TURBINE (2), NATURAL GAS	116 MW	9 PPMV	DRY LOW NOX BURNER WITH SCR	0	BACT-PSD
GEORGIA OULF CORPORATION	LA	Mar-96	GENERATOR, NATURAL GAS FIRED TURBINE	1,123 MM BTU/HR	25 PPMV CORR. TO 15% O2	CONTROL NOX USING STEAM INJECTION	0	BACT-PSD
SEMINOLE HARDEE UNIT 3	FL	Jan-96	COMBINED CYCLE COMBUSTION TURBINE	140 MW	15 PPM @ 15% O2	DRY LOW NOX COMBUSTION	0	BACT-PSD
KEY WEST CITY ELECTRIC SYSTEM	FL	Sep-95	TURBINE, EXISTING CT RELOCATION TO A NEW PLANT	23 MW	75 PPM @ 15% O2	WATER INJECTION	0	BACT-PSO
UNION CARBIDE CORPORATION	LA	Sep-95	GENERATOR, GAS TURBINE	1,313 MM BTU/HR	25 PPMV CORR. TO 15% O	DRY LOW NOX COMBUSTOR	0	BACT-PSD
PUERTO RICO ELECTRIC POWER AUTHORITY (PREPA)	PR	Jul-95	COMBUSTION TURBINES (3), 0.3 MW SIMPLE-CYCLE EACH	248 MW	35 LB/HR AS NO2	STEAM INJECTION PLUS SELECTIVE CATALYTIC REDUCTION (SCR) SYSTEM. USE OF NO. 2 FUEL OIL WITH NITROGEN CONTENT NOT TO EXCEED 0.10% BY WEIGHT.	0	BACT-PSD
HOGANSVILLE MUNICIPAL POWER FACILITY	MO	Jul-95	ADD OF A DUAL FUEL FIRED TWIN-PAC TURBINE	49 MW	42 PPM BY VOL 1 HR AVG	CONTROLS TO REGULATE THE FUEL CONSUMPTION AND THE RATIO OF WATER TO FUEL BEING FIRED IN THE TURBINES	0	BACT-PSD
HOGANSVILLE MUNICIPAL POWER FACILITY	MO	Jul-95	ADD OF A DUAL FUEL FIRED TWIN-PAC TURBINE	49 MW	75 PPM BY VOL 1 HR AVG	RATIO OF WATER TO FUEL BEING FIRED IN THE TURBINES	0	BACT-PSD
BROOKLYN NAVY YARD COOPERATION PARTNERS L.P.	NY	Jun-95	TURBINE, NATURAL GAS FIRED	240 MW	3.5 PPM @ 15% O2	SCR	0	LAER
PANDAKATHLEEN, L.P.	FL	Jun-95	COMBINED CYCLE COMBUSTION TURBINE (TOTAL 115MW)	75 MW	15 PPM @ 15% O2	DRY LOW NOX BURNER	0	BACT-PSD
PROCTOR AND GAMBLE PAPER PRODUCTS CO (CHARM)	PA	May-95	TURBINE, NATURAL GAS	580 MMBTU/HR	55 PPM @ 15% O2	STEAM INJECTION	75	RACT
MILAGRO, WILLIAMS FIELD SERVICE	NM	May-95	TURBINE/COGEN, NATURAL GAS (2)	900 MMCF/DAY	9 PPM @ 15% O2	DRY LOW NOX (GENERAL ELECTRIC MODEL PG6541B) DRY LOW NOX BURNERS GE FRAME UNIT, CAN ANNUAL	94	BACT-PSD
GAINESVILLE REGIONAL UTILITIES	FL	Apr-95	SIMPLE CYCLE COMBUSTION TURBINE, GASANO 2 OIL B-UP	74 MW	15 PPM AT 15% OXYGEN	COMBUSTORS	0	BACT-PSD
GAINESVILLE REGIONAL UTILITIES	FL	Apr-95	OIL FIRED COMBUSTION TURBINE	74 MW	42 PPM AT 15% OXYGEN	WATER INJECTION	0	BACT-PSD
LEDERLE LABORATORIES	NY	Apr-95	(2) GAS TURBINES (EP #S 00101&102)	110 MMBTU/HR	42 PPM, 18 LB/HR	STEAM INJECTION	0	BACT-PSD
PILOGRAM ENERGY CENTER	NY	Apr-95	(2) WESTINGHOUSE W50103 TURBINES (EP #S 00001&2)	1,400 MMBTU/HR	4.5 PPM, 23.6 LB/HR	STEAM INJECTION FOLLOWED BY SCR	0	BACT-PSD
BALTIMORE GAS & ELECTRIC - PERRYMAN PLANT	MD	Mar-95	TURBINE, 140 MM NATURAL GAS FIRED ELECTRIC	140 MW	15 PPM @ 15% O2	DRY BURN LOW NOX BURNERS	91	BACT-PSD
FORMOSA PLASTICS CORPORATION, LOUISIANA	LA	Mar-95	TURBINE/HSRO, GAS COGENERATION	450 MM BTU/HR	9 PPMV	DRY LOW NOX BURNER/COMBUSTION DESIGN AND CONTROL	0	LAER
LSP-COTTAGE GROVE, L.P.	MN	Mar-95	COMBUSTION TURBINE/GENERATOR	1,970 MMBTU/HR	4.5 PPM @ 15% O2 GAS	SELECTIVE CATALYTIC REDUCTION (SCR)	70	BACT-PSD
EMPIRE DISTRICT ELECTRIC CO.	MO	Feb-95	INSTALL TWO NEW SIMPLE-CYCLE TURBINES	89 MW	360 TPY	WATER INJECTION	0	BACT-PSD
MARATHON OIL CO., INDIAN BASIN N.O. PLANT	NM	Jan-95	TURBINES, NATURAL GAS (2)	5,500 HP	7.4 LB/HR	LEAN-PREMIUM COMBUSTION TECHNOLOGY. DRY LOW NOX	66	BACT-PSD
KAMNEBESICORP SYRACUSE LP	NY	Dec-94	SIEMENS V64.3 GAS TURBINE (EP #00001)	650 MMBTU/HR	25 PPM	WATER INJECTION	70	BACT
INDECK-OSWEGO ENERGY CENTER	NY	Oct-94	GE FRAME 6 GAS TURBINE	533 LB/AMBTU	42 PPM, 75.00 LB/HR	STEAM INJECTION	53	BACT
FULTON COGEN PLANT	NY	Sep-94	GE LM5000 GAS TURBINE	500 MMBTU/HR	36 PPM, 65 LB/HR	WATER INJECTION	59	BACT-PSD
CAROLINA POWER AND LIGHT	SC	Aug-94	STATIONARY GAS TURBINE	1,250 MMBTU/HR	25 PPMV @ 15% O2 (GAS)	WATER INJECTION	30	BACT-PSD
CAROLINA POWER AND LIGHT	SC	Aug-94	STATIONARY GAS TURBINE	1,520 MMBTU/HR	62 PPMV @ 15% O2 (OIL)	WATER INJECTION	74	BACT-PSD
BRUSH COGENERATION PARTNERSHIP	CO	Jul-94	TURBINE	350 MMBTU/HR	25 PPM @ 15% O2	DRY LOW NOX BURNER	0	BACT-PSD
COLORADO POWER PARTNERSHIP	CO	Jul-94	TURBINES, 2 NAT GAS & 2 DUCT BURNERS	385 MMBTU/HR EACH TURBIN	42 PPM @ 15% O2	WATER INJECTION	66	BACT-PSD
MUDDY RIVER L.P.	NV	Jun-94	COMBUSTION TURBINE, DIESEL & NATURAL GAS	140 MEGAWATT	303 LB/HR	LOW NOX BURNER	0	BACT-PSD
CSW NEVADA, INC.	NV	Jun-94	COMBUSTION TURBINE, DIESEL & NATURAL GAS	140 MEGAWATT	273 LB/HR	DRY LOW NOX COMBUSTOR	0	BACT-PSD
PORTLAND GENERAL ELECTRIC CO.	OR	May-94	TURBINES, NATURAL GAS (2)	1,720 MMBTU	4.5 PPM @ 15% O2	SCR	82	BACT-PSD
EMPIRE DISTRICT ELECTRIC CO.	MO	May-94	INSTALL TWO NEW SIMPLE-CYCLE TURBINES	1345 MMBTU/HR	25 PPM BY VOL 1 HR AVG	LOW NOX BURNERS, AND WATER INJECTION	0	BACT-PSD
EMPIRE DISTRICT ELECTRIC CO.	MO	May-94	INSTALL TWO NEW SIMPLE-CYCLE TURBINES	1,345 MMBTU/HR	1,135 TPY (NO. 2 OIL)	LOW NOX BURNERS, AND WATER INJECTION	0	BACT-PSD
GEORGIA POWER COMPANY, ROBINS TURBINE PROJECT	GA	May-94	TURBINE, COMBUSTION, NATURAL GAS	80 MW	25 PPM	WATER INJECTION, FUEL SPEC: NATURAL GAS	0	BACT-PSD
WEST CAMPUS COGENERATION COMPANY	TX	May-94	GAS TURBINES	75 MW (TOTAL POWER)	200 TPY	INTERNAL COMBUSTION CONTROLS	0	BACT-PSO
FLEETWOOD COGENERATION ASSOCIATES	PA	Apr-94	NG TURBINE (GE LM6000) WITH WASTE HEAT BOILER	360 MMBTU/HR	21 LB/HR	SCR WITH LOW NOX COMBUSTORS	47	BACT-OTHER
HERMISTON GENERATING CO.	OR	Apr-94	TURBINES, NATURAL GAS (2)	1,696 MMBTU	4.5 PPM @ 15% O2	SCR	82	BACT-PSD
FLORIDA POWER CORPORATION POLK COUNTY SITE	FL	Feb-94	TURBINE, NATURAL GAS (2)	1,510 MMBTU/HR	12 PPMV @ 15% O2	DRY LOW NOX COMBUSTOR	0	BACT-PSD
FLORIDA POWER CORPORATION POLK COUNTY SITE	FL	Feb-94	TURBINE, FUEL OIL (2)	1,730 MMBTU/HR	42 PPMV @ 15% O2	WATER INJECTION	0	BACT-PSD
TECO POLK POWER STATION	FL	Feb-94	TURBINE, SYNGAS (COAL GASIFICATION)	1,755 MMBTU/HR	25 PPMV @ 15% O2	DRY LOW NOX COMBUSTOR	0	BACT-PSD
TECO POLK POWER STATION	FL	Feb-94	TURBINE, FUEL OIL	1,765 MMBTU/HR	42 PPMV @ 15% O2	WET INJECTION	0	BACT-PSD
INTERNATIONAL PAPER	LA	Feb-94	TURBINE/HSRO, GAS COGEN	338 MM BTU/HR TURBINE	25 PPMV 15% O2 TURBINE	DRY LOW NOX COMBUSTOR/COMBUSTION CONTROL	0	BACT
KAMNEBESICORP CARTHAGE L.P.	NY	Jan-94	GE FRAME 6 GAS TURBINE	491 BTU/HR	42 PPM, 76.6 LB/HR	STEAM INJECTION	63	BACT
ORANGE COGENERATION LP	NY	Dec-93	TURBINE, NATURAL GAS, 2	368 MMBTU/HR	15 PPM @ 15% O2	DRY LOW NOX COMBUSTOR	0	BACT-PSO
PROJECT ORANGE ASSOCIATES	NY	Dec-93	GE LM-5000 GAS TURBINE	550 MMBTU/HR	25 PPM, 47 LB/HR	STEAM INJECTION, FUEL SPEC: NATURAL GAS ONLY	80	BACT
WILLIAMS FIELD SERVICES CO., EL CEDRO COMPRESSOR	NM	Oct-93	TURBINE, GAS-FIRED	11,257 HP	12 PPM @ 15% O2	SOLONOX COMBUSTOR, DRY LOW NOX TECHNOLOGY	66	BACT-PSD
FLORIDA GAS TRANSMISSION	FL	Sep-93	TURBINE, GAS	132 MMBTU/HR	25 PPM @ 15% O2	DRY LOW NOX COMBUSTOR	0	BACT-PSD

Table B-2. Summary of Best Available Control Technology (BACT) Determinations for Nitrogen Oxide (NOx) Emissions

PATOWMACK POWER PARTNERS, LIMITED PARTNERSHIP	VA	Sep-93	TURBINE, COMBUSTION, SIEMENS MODEL VM 2, 3	10.2 X109 SCF/YR NAT GAS	131 LBAR(GAS); 339 OIL	DRY LOW NOX COMBUSTOR; DESIGN, WATER INJECTION	0	BACT-PSD
FLORIDA GAS TRANSMISSION COMPANY	AL	Aug-93	TURBINE, NATURAL GAS	12,600 BHP	0.58 GMAHP HR	AR-TO-FUEL RATIO CONTROL, DRY LOW NOX COMBUSTION	71	BACT-PSD
LOCKPORT COGEN FACILITY	NY	Jul-93	(6) GE FRAME 4 TURBINES (EP #S 00001-00006)	424 MMBTUHR	42 PPM	STEAM INJECTION	78	BACT
AVTEC COGEN PLANT	NY	Jul-93	GE LM5000 COMBINED CYCLE GAS TURBINE EP #00001	451 MMBTUHR	25 PPM, 41 LBAR	NO CONTROLS	0	BACT-OTHER
NEWARK BAY COGENERATION PARTNERSHIP, L.P.	NJ	Jun-93	TURBINES, COMBUSTION, KEROSENE-FIRED (2)	640 MMBTUHR (EACH)	16 PPMVD	SCR	0	BACT-PSD
NEWARK BAY COGENERATION PARTNERSHIP, L.P.	NJ	Jun-93	TURBINES, COMBUSTION, NATURAL GAS-FIRED (2)	617 MMBTUHR (EACH)	8.3 PPMVD	SCR	0	BACT-PSD
TIGER BAY LP	FL	May-93	TURBINE, OIL	1,850 MMBTUHR	42 PPM @ 15% O2	WATER INJECTION	0	BACT-PSD
TIGER BAY LP	FL	May-93	TURBINE, GAS	1,615 MMBTUHR	15 PPM @ 15% O2	DRY LOW NOX COMBUSTOR	0	BACT-PSD
INDECK ENERGY COMPANY	NY	May-93	GE FRAME 6 GAS TURBINE EP #00001	491 MMBTUHR	32 PPM	STEAM INJECTION	58	BACT
PHOENIX POWER PARTNERS	CO	May-93	TURBINE (NATURAL GAS)	311 MMBTUHR	22 PPM @ 15% O2	DRY LOW NOX COMBUSTION	0	BACT-OTHER
TRIGEN MITCHEL FIELD	NY	Apr-93	GE FRAME 6 GAS TURBINE	425 MMBTUHR	60 PPM, 50 LBAR	STEAM INJECTION	20	BACT
KISSAMEE UTILITY AUTHORITY	FL	Apr-93	TURBINE, FUEL OIL	928 MMBTUHR	42 PPM @ 15% O2	WATER INJECTION	0	BACT-PSD
KISSAMEE UTILITY AUTHORITY	FL	Apr-93	TURBINE, FUEL OIL	371 MMBTUHR	42 PPM @ 15% O2	WATER INJECTION	0	BACT-PSD
KISSAMEE UTILITY AUTHORITY	FL	Apr-93	TURBINE, NATURAL GAS	869 MMBTUHR	15 PPM @ 15% O2	DRY LOW NOX COMBUSTOR	0	BACT-PSD
KISSAMEE UTILITY AUTHORITY	FL	Apr-93	TURBINE, NATURAL GAS	367 MMBTUHR	15 PPM @ 15% O2	DRY LOW NOX COMBUSTOR	0	BACT-PSD
EAST KENTUCKY POWER COOPERATIVE	KY	Mar-93	TURBINES (3), #2 FUEL OIL AND NAT. GAS FIRED	1,492 MMBTUHR (EACH)	42 PPM @ 15% O2 (OIL)	WATER INJECTION	46	SEE NOTES
INTERNATIONAL PAPER CO., RIVERDALE MILL	AL	Jan-93	TURBINE, STATIONARY (GAS-FIRED) WITH DUCT BURNER	40 MW	0.08 LBAR(MBTU) (GAS)	INTO THE TURBINE	0	BACT-PSD
OKLAHOMA MUNICIPAL POWER AUTHORITY	OK	Dec-92	TURBINE, COMBUSTION	58 MW	65 PPM @ 15% O2 (OIL)	COMBUSTION CONTROLS	83	BACT-OTHER
OKLAHOMA MUNICIPAL POWER AUTHORITY	OK	Dec-92	TURBINE, COMBUSTION	58 MW	25 PPM @ 15% O2 (GAS)	COMBUSTION CONTROLS	83	BACT-OTHER
AUBURNDALE POWER PARTNERS, LP	FL	Dec-92	TURBINE, OIL	1,170 MMBTUHR	42 PPMVD @ 15% O2	STEAM INJECTION	0	BACT-PSD
AUBURNDALE POWER PARTNERS, LP	FL	Dec-92	TURBINE, GAS	1,214 MMBTUHR	15 PPMVD @ 15% O2	DRY LOW NOX COMBUSTOR	0	BACT-PSD
SITH-DEPENDENCE POWER PARTNERS	NY	Nov-92	TURBINES, COMBUSTION (4) (NATURAL GAS) (1012 MW)	2,133 MMBTUHR (EACH)	4.5 PPM	SCR AND DRY LOW NOX	0	BACT-OTHER
KAMNEBESICORP BEAVER FALLS COGENERATION FACILITY	NY	Nov-92	TURBINE, COMBUSTION (NAT. GAS & OIL FUEL) (79MW)	650 MMBTUHR	9 PPM (GAS)	DRY LOW NOX OR SCR	0	BACT-OTHER
KAMNEBESICORP BEAVER FALLS COGENERATION FACILITY	NY	Nov-92	TURBINE, COMBUSTION (NAT. GAS & OIL FUEL) (79MW)	650 MMBTUHR	85 PPM (OIL)	DRY LOW NOX OR SCR	0	BACT-OTHER
KAMNEBESICORP CORNING, L.P.	NJ	Nov-92	TURBINE, COMBUSTION (79 MW)	583 MMBTUHR	9 PPM	DRY LOW NOX OR SCR	0	BACT-OTHER
GRAYS FERRY CO. GENERATION PARTNERSHIP	PA	Nov-92	TURBINE (NATURAL GAS & OIL)	1,150 MMBTU	9 PPMVD (NAT. GAS)	DRY LOW NOX BURNER, COMBUSTION CONTROL	0	BACT-OTHER
GOAL LINE, LP ICEFLOE	CA	Nov-92	TURBINE, COMBUSTION (NATURAL GAS) (42.4 MW)	386 MMBTUHR	4 PPMVD @ 15% OXYGEN	WATER INJECTION & SCR W/ AUTOMATIC AMMONIA INJECT.	98	BACT-OTHER
BEAR ISLAND PAPER COMPANY, L.P.	VA	Oct-92	TURBINE, COMBUSTION GAS	468 X10(6) BTUHR #2 OIL	15 PPM	SCR	51	BACT-PSD
BEAR ISLAND PAPER COMPANY, L.P.	VA	Oct-92	TURBINE, COMBUSTION GAS (TOTAL)	0.0	69.7 TPY	SCR	0	BACT-PSD
BEAR ISLAND PAPER COMPANY, L.P.	VA	Oct-92	TURBINE, COMBUSTION GAS	474 X10(6) BTUHR N. GAS	9 PPM	SELECTIVE CATALYTIC REDUCTION (SCR)	75	BACT-PSD
GORDONSVILLE ENERGY L.P.	VA	Sep-92	TURBINE FACILITY, GAS	7.4 X10(7) GPY FUEL OIL	245 TOTAL TPY	SELECTIVE CATALYTIC REDUCTION (SCR)	80	BACT-PSD
GORDONSVILLE ENERGY L.P.	VA	Sep-92	TURBINES (2) [EACH WITH A SF]	1.4 X10(9) SCF/YR #2 OIL	66 LBARS/HR	WATER INJECTION AND SCR	80	BACT-PSD
GORDONSVILLE ENERGY L.P.	VA	Sep-92	TURBINE FACILITY, GAS	1,331 X10(7) SCF/YR NAT GAS	245 TOTAL TPY	SELECTIVE CATALYTIC REDUCTION (SCR) W/ WATER INJECT	50	BACT-PSD
GORDONSVILLE ENERGY L.P.	VA	Sep-92	TURBINES (2) [EACH WITH A SF]	1.5 X10(9) BTUHR N. GAS	5 PPMVD/HR @ 15% O2	SCR WITH WATER INJECTION	80	BACT-PSD
NEVADA POWER COMPANY, HARRY ALLEN PEAKING PLANT	NV	Sep-92	COMBUSTION TURBINE ELECTRIC POWER GENERATION	600 MW (8 UNITS 75 EACH)	88.6 TPY (EACH TURBINE)	LOW NOX COMBUSTOR	0	BACT-PSD
KAMEL SOUTH GLENS FALLS COGEN CO	NY	Sep-92	GE FRAME 6 GAS TURBINE	498 MMBTUHR	42 PPM, 15.5 LBAR	WATER INJECTION	50	BACT
NORTHERN STATES POWER COMPANY	SD	Sep-92	TURBINE, SIMPLE CYCLE, 4 EACH	129 MW	24 PPM @ 15% O2 GAS	WATER INJECTION FOR GAS & DISTILLATION	0	BACT-PSD
PASNY/HOLTSVILLE COMBINED CYCLE PLANT	NY	Sep-92	TURBINE, COMBUSTION GAS (150 MW)	1,146 MMBTUHR (GAS)	9 PPM (GAS)	DRY LOW NOX	0	BACT-OTHER
PASNY/HOLTSVILLE COMBINED CYCLE PLANT	NY	Sep-92	TURBINE, COMBUSTION GAS (150 MW)	1,146 MMBTUHR (GAS)	42 PPM (OIL)	WATER INJECTOR	0	BACT-OTHER
WEPCU, PARIS SITE	WI	Aug-92	TURBINES, COMBUSTION (4)	0.0	65 PPM @ 15% O2 (OIL)	GOOD COMBUSTION PRACTICES	0	BACT-PSD
WEPCU, PARIS SITE	WI	Aug-92	TURBINES, COMBUSTION (4)	0.0	25 PPM @ 15% O2 (GAS)	GOOD COMBUSTION PRACTICES	0	BACT-PSD
FLORIDA POWER CORPORATION	FL	Aug-92	TURBINE, OIL	1,029 MMBTUHR	42 PPMVD @ 15% O2	WET INJECTION	0	BACT-PSD
FLORIDA POWER CORPORATION	FL	Aug-92	TURBINE, OIL	1,866 MMBTUHR	42 PPMVD @ 15% O2	WET INJECTION	0	BACT-PSD
NORTHWEST PIPELINE COMPANY	WA	Aug-92	TURBINE, GAS-FIRED	12,100 HP	196 PPM @ 15% O2	ADVANCED DRY LOW NOX COMBUSTOR (BY 07/01/95)	76	BACT-PSD
CHO TRANSMISSION	OH	Aug-92	TURBINE (NATURAL GAS) (3)	5,500 HP (EACH)	1.6 GHP-HR	LOW NOX COMBUSTION	0	BACT-OTHER
SAVANNAH ENERGY COMPANY	NY	Jul-92	TURBINE, COMBUSTION (2) (NATURAL GAS)	1,123 MMBTUHR (EACH)	9 PPM	SCR	0	BACT-OTHER
HARTWELL ENERGY LIMITED PARTNERSHIP	GA	Jul-92	TURBINE, OIL FIRED (2 EACH)	1,840 M BTUHR	25 PPMVD, FUEL N AFLOW	MAXIMUM WATER INJECTION	0	BACT-PSD
MAUI ELECTRIC COMPANY, LTD. MAALAEA GENERATING STA	HI	Jul-92	TURBINE, COMBINED-CYCLE COMBUSTION	28 MW	42.3 LBAR	WATER INJECTION	59	BACT-OTHER
HARTWELL ENERGY LIMITED PARTNERSHIP	GA	Jul-92	TURBINE, GAS FIRED (2 EACH)	1,817 M BTUHR	25 PPM @ 15% O2	MAXIMUM WATER INJECTION	0	BACT-PSD
INDECK-YERKES ENERGY SERVICES	NY	Jun-92	GE FRAME 6 GAS TURBINE (EP #00001)	432 MMBTUHR	42 PPM, 74 LBAR	STEAM INJECTION	35	BACT
SELKIRK COGENERATION PARTNERS, L.P.	NY	Jun-92	COMBUSTION TURBINES (2) (252 MW)	1,173 MMBTUHR (EACH)	9 PPM GAS	STEAM INJECTION AND SCR	0	BACT-OTHER
SELKIRK COGENERATION PARTNERS, L.P.	NY	Jun-92	COMBUSTION TURBINE (79 MW)	1,173 MMBTUHR	25 PPM GAS	STEAM INJECTION	0	BACT-OTHER
NORTHWEST PIPELINE CORPORATION	CO	May-92	TURBINE, SOLAR TAILRUS	45 MMBTUHR	95 PPMVD (UNTIL 11/98)	DRY LOW NOX COMBUSTOR (BY 11/01/98)	0	BACT-PSD
MARRAGANSETT ELECTRIC/NEW ENGLAND POWER CO.	RI	Apr-92	TURBINE, GAS AND DUCT BURNER	1,360 MMBTUHR EACH	9 PPM @ 15% O2, GAS	SCR	0	BACT-PSD
KENTUCKY UTILITIES COMPANY	KY	Mar-92	TURBINE, #2 FUEL OIL/NATURAL GAS (8)	1,500 MM BTUHR (EACH)	42 PPM @ 15% O2, N. GAS	WATER INJECTION	0	BACT-PSD
BERMUDA HUNDRED ENERGY LIMITED PARTNERSHIP	VA	Mar-92	TURBINE, COMBUSTION	1,175 MMBTUHR NAT. GAS	9 PPM @ 15% O2	SCR, STEAM INJECTION	91	BACT-PSD
BERMUDA HUNDRED ENERGY LIMITED PARTNERSHIP	VA	Mar-92	TURBINE, COMBUSTION	1,117 MMBTUHR NO2 FUEL OIL	15 PPM @ 15% O2	SCR, STEAM INJ.	91	BACT-PSD
BERMUDA HUNDRED ENERGY LIMITED PARTNERSHIP	CO	Feb-92	TURBINE, GAS FIRED, 5 EACH	0.0	191 TPA/HR	DRY LOW NOX TECH.	0	BACT-PSD
THERMO INDUSTRIES, LTD.	HI	Feb-92	TURBINE, FUEL OIL #2	246 MMBTUHR	25 PPM @ 15% O2	COMBUSTOR WATER INJECTOR, WATER INJECTION	70	BACT-PSD
HAWAII ELECTRIC LIGHT CO., INC.	HI	Feb-92	TURBINES, 8	20 MW	42.3 LBAR	MAX WATER INJECTION	0	BACT-PSD
SAVANNAH ELECTRIC AND POWER CO.	GA	Feb-92	TURBINES, 8	1,032 MMBTUHR, NAT GAS	25 PPM @ 15% O2	MAX WATER INJECTION	0	BACT-PSD
SAVANNAH ELECTRIC AND POWER CO.	GA	Feb-92	TURBINES, 8	972 MMBTUHR, #2 OIL	0 SEE NOTES	MAX WATER INJECTION	0	BACT-PSD
LINDEN COGENERATION TECHNOLOGY	NJ	Jan-92	TURBINE, NATURAL GAS FIRED	50 X E12 BTUHR	33.8 LBAR	STEAM INJECTION AND SCR	95	BACT-PSD
ALYESKA PIPELINE SERVICE COMPANY	AK	Jan-92	SOLAR CENTAUR, 3	800 KW	150 PPMVD @ 15% O2	LOW NOX BURNERS	0	NSPS
KAMNEBESICORP NATURAL DAM LP	NY	Dec-91	GE FRAME 6 GAS TURBINE	500 MMBTUHR	42 PPM, 80.1 LBAR	STEAM INJECTION	35	BACT
DUKE POWER CO. LINCOLN COMBUSTION TURBINE STATION	NC	Dec-91	TURBINE, COMBUSTION	1,247 MM BTUHR	267 LBAR	MULTINOZZLE COMBUSTOR, MAXIMUM WATER INJECTION	0	BACT-PSD
DUKE POWER CO. LINCOLN COMBUSTION TURBINE STATION	NC	Dec-91	TURBINE, COMBUSTION	1,313 MM BTUHR	119 LBAR	MULTINOZZLE COMBUSTOR, MAXIMUM WATER INJECTION	0	BACT-PSD
MALE ELECTRIC COMPANY, LTD.	HI	Dec-91	TURBINE, FUEL OIL #2	28 MW	42 PPM	WATER INJECTION	71	BACT-PSD
KALAMAZOO POWER LIMITED	MI	Dec-91	TURBINE, GAS-FIRED, 2, W/ WASTE HEAT BOILERS	1,806 MMBTUHR	15 PPMV	DRY LOW NOX TURBINES	0	BACT-PSD
LAKE COGEN LIMITED	FL	Nov-91	TURBINE, OIL, 2 EACH	42 MW	42 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
LAKE COGEN LIMITED	FL	Nov-91	TURBINE, GAS, 2 EACH	42 MW	25 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
SHELL PIPELINE CORPORATION	CA	Nov-91	GENERATOR, EMERGENCY, PROPANE FIRED	82 BHP	0.28 LBAR	3-WAY CATALYTIC CONVERTER	60	BACT-PSD
DE LA GUERRA POWER, INC	CA	Nov-91	ENGINE IC & GEN (1 OF 3)	380 HP	6.34 LBO	NON-SELECTIVE CATALYTIC CONVERTER	90	BACT-PSD
ORLANDO UTILITIES COMMISSION	FL	Nov-91	TURBINE, GAS, 4 EACH	35 MW	42 PPM @ 15% O2	WET INJECTION	70	BACT-PSD
ORLANDO UTILITIES COMMISSION	FL	Nov-91	TURBINE, OIL, 4 EACH	35 MW	65 PPM @ 15% O2	WET INJECTION	0	BACT-PSD
SOUTHERN CALIFORNIA GAS	CA	Oct-91	TURBINE, GAS FIRED, SOLAR MODEL H	5,500 HP	8 PPM @ 15% O2	HIGH TEMP SELECT. CAT. REDUCTION	93	BACT-PSD
EL PASO NATURAL GAS	AZ	Oct-91	TURBINE, GAS, SOLAR CENTAUR H	5,500 HP	84.9 PPM @ 15% O2	LEAN BURN	0	NSPS
EL PASO NATURAL GAS	AZ	Oct-91	TURBINE, GAS, SOLAR CENTAUR H	5,500 HP	42 PPM @ 15% O2	DRY LOW NOX COMBUSTOR	51	BACT-PSD
EL PASO NATURAL GAS	AZ	Oct-91	TURBINE, GAS, SOLAR CENTAUR H	5,500 HP	81.1 PPM @ 15% O2	FUEL SPEC. LEAN FUEL MIX	0	NSPS
EL PASO NATURAL GAS	AZ	Oct-91	TURBINE, GAS, SOLAR CENTAUR H	5,500 HP	42 PPM @ 15% O2	DRY LOW NOX COMBUSTOR	0	BACT-PSD
FLORIDA POWER GENERATION	FL	Oct-91	TURBINE, OIL, 4 EACH	93 MW	42 PPM @ 15% O2	WET INJECTION	0	BACT-PSD
EL PASO NATURAL GAS	AZ	Oct-91	TURBINE, NAT. GAS TRANSM., GE FRAME 3	12,000 HP	225 PPM @ 15% O2	LEAN BURN	0	BACT-PSD
EL PASO NATURAL GAS	AZ	Oct-91	TURBINE, NAT. GAS TRANSM., GE FRAME 3	12,000 HP	42 PPM @ 15% O2	DRY LOW NOX COMBUSTOR	80	BACT-PSD
NUGGET OIL CO.	CA	Oct-91	GENERATOR, STEAM, GAS FIRED	63 MMBTUHR	0.043 LBAR(MBTU)	LOW NOX BURNER AND FLUE GAS RECIRCULATION	57	BACT-PSD
CAROLINA POWER AND LIGHT CO.	SC	Sep-91	TURBINE, I.C.	60 MW	292 LBAR	WATER INJECTION	50	BACT-PSD
ENRON LOUISIANA ENERGY COMPANY	LA	Aug-91	TURBINE, GAS, 2	39 MMBTUHR	40 PPM @ 15% O2	H2O INJECT 0.67 LBAR	71	BACT-PSD
ALCONOURN GAS TRANSMISSION CO.	RI	Jul-91	TURBINE, GAS, 2	49 MMBTUHR	100 PPM @ 15% O2	LOW NOX COMBUSTION	0	BACT-OTHER

Table B-2. Summary of Best Available Control Technology (BACT) Determinations for Nitrogen Oxide (NOx) Emissions

CHARLES LARSEN POWER PLANT	FL	Jul-91	TURBINE, OIL, 1 EACH	80 MW	42 PPM @ 15% O2	WET INJECTION	0	BACT-PSD
CHARLES LARSEN POWER PLANT	FL	Jul-91	TURBINE, GAS, 1 EACH	80 MW	25 PPM @ 15% O2	WET INJECTION	0	BACT-PSD
SUMAS ENERGY INC.	WA	Jun-91	TURBINE, NATURAL GAS	88 MW	6 PPM @ 15% O2	SCR	90	BACT-PSD
SAGUARO POWER COMPANY	NV	Jun-91	COMBUSTION TURBINE GENERATOR	35 MW	16.9 PPM (WINTER)	SELECTIVE CATALYTIC REDUCTION (SCR)	80	BACT-PSD
FLORIDA POWER AND LIGHT	FL	Jun-91	TURBINE, OIL, 2 EACH	400 MW	65 PPM @ 15% O2	LOW NOX COMBUSTORS	0	BACT-PSD
FLORIDA POWER AND LIGHT	FL	Jun-91	TURBINE, GAS, 4 EACH	400 MW	25 PPM @ 15% O2	LOW NOX COMBUSTORS	0	BACT-PSD
FLORIDA POWER AND LIGHT	FL	Jun-91	TURBINE, CO, 4 EACH	400 MW	42 PPM @ 15% O2	LOW NOX COMBUSTORS	0	BACT-PSD
GRANITE ROAD LIMITED	CA	May-91	TURBINE, GAS, ELECTRIC GENERATION	451 MMBTU/Hr	3.5 PPM @ 15% O2	SCR, STEAM INJECTION	97	BACT-PSD
NORTHERN CONSOLIDATED POWER	PA	May-91	TURBINES, GAS, 2	35 KW EACH	25 PPM @ 15% O2	STEAM INJECTION+SCR IN 1997	95	OTHER
CMARRON CHEMICAL	CO	Mar-91	TURBINE #1, GE FRAME 6	33 MW	25 PPM @ 15% O2	WATER INJECTION	0	OTHER
CMARRON CHEMICAL	CO	Mar-91	TURBINE #2, GE FRAME 6	33 MW	9 PPM @ 15% O2	SCR	0	OTHER
SEMOLE FERTILIZER CORPORATION	FL	Mar-91	TURBINE, GAS	26 MW	9 PPM @ 15% O2	SCR	0	BACT-PSD
FLORIDA POWER AND LIGHT	FL	Mar-91	TURBINE, GAS, 4 EACH	240 MW	42 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
FLORIDA POWER AND LIGHT	FL	Mar-91	TURBINE, OIL, 4 EACH	0.0	65 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
CITY UTILITIES OF SPRINGFIELD	MO	Mar-91	GENERATION OF ELECTRICAL POWER	752 MMBTU/Hr	42 PPM BY VOL 1 HR AVG	WATER INJECTION	0	BACT-PSD
CITY UTILITIES OF SPRINGFIELD	MO	Mar-91	GENERATION OF ELECTRICAL POWER	752 MMBTU/Hr	65 PPM BY VOL 1 HR AVG	WATER INJECTION	0	BACT-PSD
CITY UTILITIES OF SPRINGFIELD	MO	Mar-91	GENERATION OF ELECTRICAL POWER	585 MMBTU/Hr	42 PPM BY VOL 1 HR AVG	WATER INJECTION	0	BACT-PSD
CITY UTILITIES OF SPRINGFIELD	MO	Mar-91	GENERATION OF ELECTRICAL POWER	585 MMBTU/Hr	65 PPM BY VOL 1 HR AVG	WATER INJECTION	0	BACT-PSD
NEVADA COGENERATION ASSOCIATES #2	NV	Jan-91	COMBINED-CYCLE POWER GENERATION	85 MW POWER OUTPUT	61.3 LBS/HR	SELECTIVE CATALYTIC SYSTEM ON ONE UNIT	0	BACT-PSD
NEVADA COGENERATION ASSOCIATES #1	NV	Jan-91	COMBINED-CYCLE POWER GENERATION	85 MW TOTAL OUTPUT	61.3 LBS/HR	SELECTIVE CATALYTIC SYSTEM ON ONE UNIT	0	BACT-PSD
NEWARK BAY COGENERATION PARTNERSHIP	NJ	Nov-90	TURBINE, NATURAL GAS FIRED	585 MMBTU/Hr	0.033 LB/MMBTU	STEAM INJECTION AND SCR	94	BACT-PSD
NORTHERN NATURAL GAS COMPANY	IA	Sep-90	ENGINE, COMPRESSOR	4,000 HP	1.8 G/G-HP-H	GOOD COMBUSTION PRACTICES	0	BACT-PSD
NORTHERN NATURAL GAS COMPANY	IA	Sep-90	ENGINE'S, COMPRESSOR, 2	2,000 HP EACH	1.8 G/G-HP-H	GOOD COMBUSTION PRACTICES	0	BACT-PSD
TBG COGEN COGENERATION PLANT	NY	Aug-90	GE LM2500 GAS TURBINE	215 MMBTU/Hr	75 PPM + FBN CORRECTIO	WATER INJECTION	60	BACT
PEPCO - CHALK POINT PLANT	MD	Jun-90	TURBINE, 105 MW NATURAL GAS FIRED ELECTRIC	105 MW	77 PPM @ 15% O2	DRY PREMIX AND WATER INJECTION	0	BACT-PSD
PEPCO - CHALK POINT PLANT	MD	Jun-90	TURBINE, 84 MW NATURAL GAS FIRED ELECTRIC	84 MW	25 PPM @ 15% O2	QUIET COMBUSTION AND WATER INJECTION	0	BACT-PSD
PACIFIC GAS TRANSMISSION COMPANY	OR	Jun-90	TURBINE GAS, COMPRESSOR STATION	110 MMBTU/Hr	199 PPM @ 15% O2	LOW NOX BURNER DESIGN	30	NSPS
PEPCO - STATION A	MD	May-90	TURBINE, 124 MW NATURAL GAS FIRED	125 MW	42 PPM @ 15% O2	WATER INJECTION	0	BACT-PSD
PEDRICKTOWN COGENERATION LIMITED PARTNERSHIP	NJ	Feb-90	TURBINE, NATURAL GAS FIRED	1,000 MMBTU/Hr	0.044 LB/MMBTU	STEAM INJECTION AND SCR	93	BACT-PSD
SC ELECTRIC AND GAS COMPANY - HAGOOD STATION	SC	Dec-89	INTERNAL COMBUSTION TURBINE	110 MEGAWATTS	308 LBS/HR	WATER INJECTION	0	BACT-PSD
PEABODY MUNICIPAL LIGHT PLANT	MA	Nov-89	TURBINE, 38 MW NATURAL GAS FIRED	412 MMBTU/Hr	25 PPM @ 15% O2	WATER INJECTION	0	BACT-OTHER
PACIFIC GAS TRANSMISSION	OR	Nov-89	TURBINE, NAT. GAS	14,500 HP	42 PPM @ 15% O2	LOW NOX BURNERS	75	BACT-PSD
SOUTHERN MARYLAND ELECTRIC COOPERATIVE (SMECO)	MD	Oct-89	TURBINE, NATURAL GAS FIRED ELECTRIC	90 MW	159 LBS/HR	WATER INJECTION	0	BACT-PSD
KINGSBURG ENERGY SYSTEMS	CA	Sep-89	TURBINE, NATURAL GAS FIRED, DUCT BURNER	35 MW	6 PPM @ 15% O2	SCR, STEAM INJECTION	90	BACT-PSD
MEGAN-RACINE ASSOCIATES, INC	NY	Aug-89	GE LM5000-N COMBINED CYCLE GAS TURBINE	401 LB/MMBTU	42 PPM @ 15% O2	WATER INJECTION	60	BACT

Note: PSD= Prevention of Significant Deterioration
 BACT= Best Available Control Technology
 LAER= Lowest Achievable Emission Rate

Table B-3. Capital Cost for Selective Catalytic Reduction for General Electric Frame "F" Simple Cycle Combustion Turbine

Cost Component	Costs	Basis of Cost Component
Direct Capital Costs		
SCR Associated Equipment	\$825,252	Vendor Based Estimate
Ammonia Storage Tank	\$134,225	\$35 per 1,000 lb mass flow developed from vendor quotes
Flue Gas Cooling	\$260,000	Vendor Based Estimate (110,000 acfm)
Instrumentation	\$82,525	10% of SCR Associated Equipment
Taxes	\$197,007	6% of SCR Associated Equipment and Catalyst
Freight	\$164,172	5% of SCR Associated Equipment and Catalyst
Total Direct Capital Costs (TDCC)	\$1,663,182	
Recurring Capital Costs (RCC)	\$2,458,197	Catalyst; Vendor Based Estimate
TOTAL CAPITAL COSTS (TCC)	\$2,919,595	Sum of TDCC and RCC
Direct Installation Costs		
Foundation and supports	\$329,710	8% of TCC; OAQPS Cost Control Manual
Handling & Erection	\$576,993	14% of TCC; OAQPS Cost Control Manual
Electrical	\$164,855	4% of TCC; OAQPS Cost Control Manual
Piping	\$82,428	2% of TCC; OAQPS Cost Control Manual
Insulation for ductwork	\$41,214	1% of TCC; OAQPS Cost Control Manual
Painting	\$41,214	1% of TCC; OAQPS Cost Control Manual
Site Preparation	\$5,000	Engineering Estimate
Buildings	\$15,000	Engineering Estimate
Total Direct Installation Costs (TDIC)	\$1,256,414	
Total Direct Capital Costs (TDCC)	\$4,176,009	
Indirect Costs		
Engineering	\$291,960	10% of Total Capital Costs; OAQPS Cost Control Manual
PSM/RMP Plan	\$25,000	Engineering Estimate
Construction and Field Expense	\$145,980	5% of Total Capital Costs; OAQPS Cost Control Manual
Contractor Fees	\$291,960	10% of Total Capital Costs; OAQPS Cost Control Manual
Start-up	\$58,392	2% of Total Capital Costs; OAQPS Cost Control Manual
Performance Tests	\$29,196	1% of Total Capital Costs; OAQPS Cost Control Manual
Allowance for Funds Used During Construction (AFU)	\$157,111	2.5% of Total Capital Costs; borrowed at a rate of 7.0% for 9 months.
Contingencies	\$87,588	3% of Total Capital Costs; OAQPS Cost Control Manual
TOTAL INDIRECT CAPITAL COST (TICC)	\$1,087,185	
TOTAL DIRECT and INDIRECT CAPITAL COSTS (TDICC)	\$5,263,194	Sum of TDCC and TDIC

Table B-4. Annualized Cost for Selective Catalytic Reduction for General Electric Frame "F" Simple Cycle Operation

Cost Component	Costs	Basis of Cost Component
Direct Annual Costs		
Operating Personnel	\$24,960	24 hours/week at \$20/hr
Supervision	\$3,744	15% of Operating Personnel; OAQPS Cost Control Manual
Maintenance - Labor	\$13,104	0.5 hr per shift, \$24/hr; OAQPS Cost Manual
- Materials	\$13,104	100% of maintenance labor; OAQPS Cost Manual
Ammonia	\$65,856	\$300 per ton NH ₃ Aqueous
PSM/RMP Update	\$5,000	Engineering Estimate
Inventory Cost	\$89,970	Capital Recovery (10.98%) for 1/3 catalyst
Catalyst Disposal Cost	\$35,793	\$28/1,000 lb/hr mass flow over 3 years; developed from vendor quotes
Contingency	\$7,546	3% of Direct Annual Costs
Total Direct Annual Costs (TDAC)	\$259,078	
Energy Costs		
Electrical	\$47,460	80kW/h for SCR; 200 kW/h for cooling fan @ \$0.05/kWh times Capacity Factor
Heat Rate Penalty	\$241,210	0.5% of MW output; EPA, 1993 (Page 6-20); plus fuel costs at \$3/mmBtu
MW Loss Penalty	\$78,611	3 days lost energy costs @ \$0.05 kWh each three period; minus fuel costs at \$3/mmBtu
Fuel Escalation	\$8,660	Escalation of fuel over inflation; 3% of energy costs
Contingency	\$11,278	3% of Energy Costs
Total Energy Costs (TEC)	\$387,219	
Indirect Annual Costs		
Overhead	\$17,222	60% of Operating/Supervision Labor and Ammonia
Property Taxes, Insurance, Admin.	\$210,528	4% of Total Capital Costs
Annualized Total Direct Capital	\$439,944	10.98% Capital Recovery Factor of 7% over 15 years times sum of TDCC, TDIC and TI
Annualized Total Direct Recurring	\$936,700	38.11% Capital Recovery Factor of 7% over 3 years times RCC
Total Indirect Annual Costs (TIAC)	\$1,604,395	
TOTAL ANNUALIZED COSTS	\$2,250,692	Sum of TDAC, TEC and TIAC
COST EFFECTIVENESS (\$ per ton removed)	\$14,886	NO _x Only
	\$25,267	All Pollutants

Table B-4. Summary of Best Available Control Technology (BACT) Determinations for Carbon Monoxide (CO) Emissions

Facility Name	State	Permit Issue Date	Unit/Process Description	Capacity (size)	CO Emission Limit	Control Method	Efficiency (%)	Type
BUCKNELL UNIVERSITY	PA	Nov-97	NO FIRE TURBINE, SOLAR TAURUS T-700S	5 MW	50 PPMV @ 15% O ₂	GOOD COMBUSTION DRY LOW-NOX TECHNOLOGY BY MAINTAINING PROPER AIR-FUEL RATIO.	0	BACT-OTHER
LORDSBURG L.P.	NM	Jun-97	TURBINE, NATURAL GAS-FIRED, ELEC. GEN.	100 MW	27 LBS/HR	GOOD COMBUSTION PRACTICES TO MINIMIZE EMISSIONS	0	BACT-PSD
MEAD COATED BOARD, INC.	AL	Mar-97	COMBINED CYCLE TURBINE (25 MW)	250 MMBTU/HR	28 PPMV @ 15% O ₂ (GAS)	PROPER DESIGN AND GOOD COMBUSTION PRACTICES	0	BACT-PSD
FORMOSA PLASTICS CORPORATION, BATON ROUGE PLANT	LA	Mar-97	TURBINE/HRSG, GAS COGENERATION	450 MM BTU/HR	70 LBS/HR	COMBUSTION DESIGN AND CONSTRUCTION.	0	BACT-PSD
SOUTHWESTERN PUBLIC SERVICE COMPANY/CUNNINGHAM STA	NM	Feb-97	COMBUSTION TURBINE, NATURAL GAS	100 MW	0 SEE FACILITY NOTES	GOOD COMBUSTION PRACTICES	0	BACT-PSD
SOUTHWESTERN PUBLIC SERVICE CO/CUNNINGHAM STATION	NM	Nov-96	COMBUSTION TURBINE, NATURAL GAS	100 MW	0 SEE P2	GOOD COMBUSTION PRACTICES	0	BACT-PSD
ECOELECTRICAL, L.P.	PR	Oct-96	TURBINES, COMBINED-CYCLE COGENERATION	461 MW	33 PPMV	COMBUSTION CONTROLS.	0	BACT-PSD
ECOELECTRICAL, L.P.	PR	Oct-96	TURBINES, COMBINED-CYCLE COGENERATION	461 MW	100 PPMV AT MIN. LOAD	COMBUSTION CONTROLS.	0	BACT-PSD
BLUE MOUNTAIN POWER, LP	PA	Jul-96	COMBUSTION TURBINE WITH HEAT RECOVERY BOILER	153 MW	3.1 PPM @ 15% O ₂	OXIDATION CATALYST 18 PPM @ 15% O ₂ WHEN FIRING NO. 2 OIL AT 75% NO LIMIT SET TO 22.1 PPM	80	OTHER
COMMONWEALTH CHESAPEAKE CORPORATION	VA	May-96	3 COMBUSTION TURBINES (OIL-FIRED)	6,000 HRS/YR	96 TPY	GOOD COMBUSTION OPERATING PRACTICES	0	BACT-NSPS
PORTSIDE ENERGY CORP.	IN	May-96	TURBINE, NATURAL GAS-FIRED	63 MEGAWATT	43 LBS/HR	15% OXYGEN, GOOD COMBUSTION AND EMISSIONS NOT TO EXCEED 10 PPMV AT 15% OXYGEN.	0	BACT-PSD
PORTSIDE ENERGY CORP.	IN	May-96	TURBINE, NATURAL GAS-FIRED	63 MEGAWATT	12 LBS/HR	15% OXYGEN, GOOD COMBUSTION PRACTICES TO MINIMIZE EMISSIONS	0	BACT-PSD
GENERAL ELECTRIC GAS TURBINES	SC	Apr-96	I.C. TURBINE	2,700 MMBTU/HR	27,169 LBS/HR	GOOD COMBUSTION PRACTICES TO MINIMIZE EMISSIONS	0	BACT-PSD
CAROLINA POWER & LIGHT	NC	Apr-96	COMBUSTION TURBINE, 4 EACH	1,908 MMBTU/HR	81 LBS/HR	COMBUSTION CONTROL	0	BACT-PSD
CAROLINA POWER & LIGHT	NC	Apr-96	COMBUSTION TURBINE, 4 EACH	1,908 MMBTU/HR	80 LBS/HR	COMBUSTION CONTROL	0	BACT-PSD
SOUTH MISSISSIPPI ELECTRIC POWER ASSOC.	MS	Apr-96	COMBUSTION TURBINE, COMBINED CYCLE	1,299 MMBTU/HR NAT GAS	26.3 PPM @ 15% O ₂ , GAS	GOOD COMBUSTION CONTROLS	0	BACT-PSD
MID-GEORGIA COGEN.	GA	Apr-96	COMBUSTION TURBINE (2), FUEL OIL	116 MW	30 PPMV	COMPLETE COMBUSTION	0	BACT-PSD
MID-GEORGIA COGEN.	GA	Apr-96	COMBUSTION TURBINE (2), NATURAL GAS	116 MW	10 PPMV	COMPLETE COMBUSTION	0	BACT-PSD
GEORGIA GULF CORPORATION	LA	Mar-96	GENERATOR, NATURAL GAS FIRED TURBINE	1,123 MM BTU/HR	972 TYP CAP FOR 3 TURB.	GOOD COMBUSTION PRACTICE AND PROPER OPERATION	0	BACT-PSD
SEMINOLE HARDEE UNIT 3	FL	Jan-96	COMBINED CYCLE COMBUSTION TURBINE	140 MW	20 PPM (NAT. GAS)	DRY LNB GOOD COMBUSTION PRACTICES	0	BACT-PSD
KEY WEST CITY ELECTRIC SYSTEM	FL	Sep-95	TURBINE, EXISTING CT RELOCATION TO A NEW PLANT	23 MW	20 PPM @ 15% O ₂ FULL LOAD	GOOD COMBUSTION	0	BACT-PSD
UNION CARBIDE CORPORATION	LA	Sep-95	GENERATOR, GAS TURBINE	1,313 MM BTU/HR	199 LBS/HR	NO ADD-ON CONTROL GOOD COMBUSTION PRACTICE	0	BACT-PSD
PUERTO RICO ELECTRIC POWER AUTHORITY (PREPA)	PR	Jul-95	COMBUSTION TURBINES (3), 83 MW SIMPLE-CYCLE EACH	248 MW	20 LBS/HR	GOOD COMBUSTION PRACTICES.	0	BACT-PSD
PUERTO RICO ELECTRIC POWER AUTHORITY (PREPA)	PR	Jul-95	COMBUSTION TURBINES (3), 83 MW SIMPLE-CYCLE EACH	248 MW	104 LBS/HR	MAINTAIN EACH TURBINE IN GOOD WORKING ORDER AND IMPLEMENT GOOD COMBUSTION PRACTICES.	0	BACT-PSD
BROOKLYN NAVY YARD COGENERATION PARTNERS L.P.	NY	Jun-95	TURBINE, NATURAL GAS FIRED	240 MW	4 PPM @ 15% O ₂	COMBUSTION CONTROLS STANDARD ONLY APPLIES IF GE CT IS SELECTED, THE ABB CT WAS LESS THAN SIGNIFICANT EMIS. INCR FOR CO	0	LAER
PANDA-KATHLEEN, L.P.	FL	Jun-95	COMBINED CYCLE COMBUSTION TURBINE (TOTAL 115M)	75 MW	25 PPM @ 15% O ₂	GOOD COMBUSTION PRACTICES	0	BACT-PSD
MILAGRO, WILLIAMS FIELD SERVICE	NM	May-95	TURBINE/COGEN, NATURAL GAS (2)	900 MMCF/DAY	28 PPM @ 15% O ₂	GOOD COMBUSTION PRACTICES	0	BACT-PSD
LEDERLE LABORATORIES	NY	Apr-95	(2) GAS TURBINES (EP #5 00101&102)	110 MMBTU/HR	46 PPM, 12.8 LBS/HR	GOOD COMBUSTION PRACTICES	0	BACT-OTHER
PILGRIM ENERGY CENTER	NY	Apr-95	(2) WESTINGHOUSE W601S TURBINES (EP #5 00001&2)	1,400 MMBTU/HR	10 PPM, 20.0 LBS/HR	GOOD COMBUSTION PRACTICES	0	BACT-OTHER
BALTIMORE GAS & ELECTRIC - PERRYMAN PLANT	MD	Mar-95	TURBINE, 140 MW NATURAL GAS FIRED ELECTRIC	140 MW	20 PPM @ 15% O ₂	GOOD COMBUSTION PRACTICES	0	BACT-PSD
FORMOSA PLASTICS CORPORATION, LOUISIANA	LA	Mar-95	TURBINE/HRSG, GAS COGENERATION	450 MM BTU/HR	26 LBS/HR	PROPER OPERATION	0	BACT-PSD
EMPIRE DISTRICT ELECTRIC CO.	MO	Feb-95	INSTALL TWO NEW SIMPLE-CYCLE TURBINES	55 MW	89 TYP	GOOD COMBUSTION CONTROL	0	BACT-PSD
MARATHON OIL CO. - INDIAN BASIN H.G. PLANT	NM	Jan-95	TURBINES, NATURAL GAS (2)	5,500 HP	43 LBS/HR	LEAN-PREMIUM COMBUSTION TECHNOLOGY.	68	BACT-PSD
KAMINE/BESICORP SYRACUSE LP	NY	Dec-94	SIEMENS V64.3 GAS TURBINE (EP #00001)	650 MMBTU/HR	9.5 PPM	NO CONTROLS	0	BACT-OTHER
INDECK-OSWEGO ENERGY CENTER	NY	Oct-94	GE FRAME 8 GAS TURBINE	533 LBS/MMBTU	10 PPM, 10.00 LBS/HR	NO CONTROLS	0	BACT-OTHER
FULTON COGEN PLANT	NY	Sep-94	GE LM5000 GAS TURBINE	500 MMBTU/HR	107 PPM, 120 LBS/HR	NO CONTROLS	0	BACT-OTHER
CAROLINA POWER AND LIGHT	SC	Aug-94	STATIONARY GAS TURBINE	1,520 MMBTU/HR	702 LBS/HR	PROPER OPERATION TO ACHIEVE GOOD COMBUSTION	0	BACT-PSD
CAROLINA POWER AND LIGHT	SC	Aug-94	STATIONARY GAS TURBINE	1,520 MMBTU/HR	414 LBS/HR	PROPER OPERATION TO ACHIEVE GOOD COMBUSTION	0	BACT-PSD
SHYDER OIL CORPORATION-RIVERTON DOME GAS PLANT	WY	Jul-94	NATURAL GAS-FIRED COMPRESSOR ENGINE	520 HORSEPOWER	1.7 LBS/HR	GOOD COMBUSTION	0	BACT
SHYDER OIL CORPORATION-RIVERTON DOME GAS PLANT	WY	Jul-94	2 GAS-FIRED GENERATOR ENGINES	365 HORSEPOWER	1.3 LBS/HR	GOOD COMBUSTION	0	BACT
SHYDER OIL CORPORATION-RIVERTON DOME GAS PLANT	WY	Jul-94	1 GAS-FIRED GENERATOR ENGINE	577 HORSEPOWER	1.9 LBS/HR	GOOD COMBUSTION	0	BACT
COLORADO POWER PARTNERSHIP	CO	Jun-94	TURBINES, 2 NAT GAS & 2 DUCT BURNERS	365 MMBTU/HR EACH TURBINE	22 PPM @ 15% O ₂	GOOD COMBUSTION	0	BACT-PSD
MUDJOY RIVER L.P.	NV	Jun-94	COMBUSTION TURBINE, DIESEL & NATURAL GAS	140 MEGAWATT	77 LBS/HR	FUEL SPEC: NATURAL GAS	0	BACT-PSD
CSW NEVADA, INC.	NV	Jun-94	COMBUSTION TURBINE, DIESEL & NATURAL GAS	140 MEGAWATT	83 LBS/HR	FUEL SPEC: NATURAL GAS	0	BACT-PSD
PORTLAND GENERAL ELECTRIC CO.	OR	May-94	TURBINES, NATURAL GAS (2)	1,700 MMBTU	15 PPM @ 15% O ₂	GOOD COMBUSTION PRACTICES	0	BACT-PSD
EMPIRE DISTRICT ELECTRIC CO.	MO	May-94	INSTALL TWO NEW SIMPLE-CYCLE TURBINES	1,345 MMBTU/HR	120 TYP	NONE	0	BACT-PSD
EMPIRE DISTRICT ELECTRIC CO.	MO	May-94	INSTALL TWO NEW SIMPLE-CYCLE TURBINES	1,345 MMBTU/HR	1200 TYP	NONE	0	BACT-PSD
NAVY PUBLIC WORKS CENTER	VA	May-94	1 EMERGENCY GENERATOR	1,500 KW	14.4 TYP	RETARD TIMING 8 DEGREES	0	NSPS
WEST CAMPUS COGENERATION COMPANY	TX	May-94	GAS TURBINES	75 MW (TOTAL POWER)	300 TYP	INTERNAL COMBUSTION CONTROLS	0	BACT
HERMISTON GENERATING CO.	OR	Apr-94	TURBINES, NATURAL GAS (2)	1,806 MMBTU	15 PPM @ 15% O ₂	GOOD COMBUSTION PRACTICES	0	BACT-PSD
FLORIDA POWER CORPORATION POLK COUNTY SITE	FL	Feb-94	TURBINE, NATURAL GAS (2)	1,510 MMBTU/HR	25 PPMV	GOOD COMBUSTION PRACTICES	0	BACT-PSD
FLORIDA POWER CORPORATION POLK COUNTY SITE	FL	Feb-94	TURBINE, FUEL OIL (2)	1,730 MMBTU/HR	30 PPMV	GOOD COMBUSTION PRACTICES	0	BACT-PSD
TECO POLK POWER STATION	FL	Feb-94	TURBINE, SYNGAS (COAL GASIFICATION)	1,755 MMBTU/HR	25 PPMV	GOOD COMBUSTION	0	BACT-PSD
TECO POLK POWER STATION	FL	Feb-94	TURBINE, FUEL OIL	1,765 MMBTU/HR	40 PPMV	GOOD COMBUSTION	0	BACT-PSD
INTERNATIONAL PAPER	LA	Feb-94	TURBINE/HRSG, GAS COGEN	338 MM BTU/HR TURBINE	166 LBS/HR	COMBUSTION CONTROL	0	BACT
KAMINE/BESICORP CARTHAGE L.P.	NY	Jan-94	GE FRAME 8 GAS TURBINE	491 BTU/HR	10 PPM, 11.0 LBS/HR	NO CONTROLS	0	BACT-OTHER
ORANGE COGENERATION LP	FL	Dec-93	TURBINE, NATURAL GAS, 2	368 MMBTU/HR	30 PPMV	GOOD COMBUSTION	0	BACT-PSD
PROJECT ORANGE ASSOCIATES	NY	Dec-93	GE LM-5000 GAS TURBINE	550 MMBTU/HR	92 LBS/HR TEMP + 20F	NO CONTROLS	0	BACT-OTHER
WILLIAMS FIELD SERVICES CO. - EL CEDRO COMPRESSOR	NM	Oct-93	TURBINE, GAS-FIRED	11,257 HP	50 PPM @ 15% O ₂	COMBUSTION CONTROL	0	BACT-PSD
PATONMACK POWER PARTNERS, LIMITED PARTNERSHIP	VA	Sep-93	TURBINE, COMBUSTION, SIEMENS MODEL V64.2, 3	10.2 X109 SCF/YR NAT GAS	26 LBS/HR	GOOD COMBUSTION OPERATING PRACTICES	0	BACT-PSD
FLORIDA GAS TRANSMISSION COMPANY	AL	Aug-93	TURBINE, NATURAL GAS	12,600 BHP	0.42 GWHP HR	AIR-TO-FUEL RATIO CONTROL, DRY COMBUSTION CONTROLS	0	BACT-PSD
LOCKPORT COGEN FACILITY	NY	Jul-93	(8) GE FRAME 8 TURBINES (EP #5 00001-00008)	424 MMBTU/HR	10 PPM	NO CONTROLS	0	BACT-OTHER
AMTEC COGEN PLANT	NY	Jul-93	GE LM5000 COMBINED CYCLE GAS TURBINE EP #00001	451 MMBTU/HR	38 PPM, 39 LBS/HR	BAFFLE CHAMBER	80	SEE NOTE #4
NEWARK BAY COGENERATION PARTNERSHIP, L.P.	NJ	Jun-93	TURBINES, COMBUSTION, KEROSENE-FIRED (2)	640 MMBTU/HR (EACH)	2.8 PPMV	OXIDATION CATALYST	0	OTHER
NEWARK BAY COGENERATION PARTNERSHIP, L.P.	NJ	Jun-93	TURBINES, COMBUSTION, NATURAL GAS-FIRED (2)	617 MMBTU/HR (EACH)	1.8 PPMV	OXIDATION CATALYST	0	OTHER
PSI ENERGY, INC. WABASH RIVER STATION	IN	May-93	COMBINED CYCLE SYNGAS TURBINE	1,775 MMBTU/HR	15 LESS THAN PPM	SYNGAS TURBINE	0	BACT-PSD
TIGER BAY LP	FL	May-93	TURBINE, OIL	1,850 MMBTU/HR	98.4 LBS/HR	GOOD COMBUSTION PRACTICES	0	BACT-PSD
TIGER BAY LP	FL	May-93	TURBINE, GAS	1,815 MMBTU/HR	49 LBS/HR	GOOD COMBUSTION PRACTICES	0	BACT-PSD
TRIGEN ENERGY COMPANY	NY	May-93	GE FRAME 8 GAS TURBINE EP #00001	491 MMBTU/HR	40 PPM	NO CONTROLS	0	BACT-OTHER
TRIGEN MITCHELL FIELD	NY	Apr-93	GE FRAME 8 GAS TURBINE	425 MMBTU/HR	10 PPM, 10.0 LBS/HR	NO CONTROLS	0	BACT-OTHER
KISSIMMEE UTILITY AUTHORITY	FL	Apr-93	TURBINE, FUEL OIL	928 MMBTU/HR	65 LBS/HR	GOOD COMBUSTION PRACTICES	0	BACT-PSD
KISSIMMEE UTILITY AUTHORITY	FL	Apr-93	TURBINE, FUEL OIL	371 MMBTU/HR	76 LBS/HR	GOOD COMBUSTION PRACTICES	0	BACT-PSD
KISSIMMEE UTILITY AUTHORITY	FL	Apr-93	TURBINE, NATURAL GAS	869 MMBTU/HR	54 LBS/HR	GOOD COMBUSTION PRACTICES	0	BACT-PSD
KISSIMMEE UTILITY AUTHORITY	FL	Apr-93	TURBINE, NATURAL GAS	367 MMBTU/HR	40 LBS/HR	GOOD COMBUSTION PRACTICES	0	BACT-PSD
EAST KENTUCKY POWER COOPERATIVE	KY	Mar-93	TURBINES (5), #2 FUEL OIL AND NAT. GAS FIRED	1,492 MMBTU/HR (EACH)	75 LBS/HR (EACH)	PROPER COMBUSTION TECHNIQUES	0	BACT-OTHER
INTERNATIONAL PAPER CO. RIVERDALE MILL	AL	Jan-93	TURBINE, STATIONARY (GAS-FIRED) WITH DUCT BURNER	40 MW	22 LBS/HR	DESIGN	0	BACT-PSD
AUBURNDALE POWER PARTNERS, LP	FL	Dec-92	TURBINE, OIL	1,170 MMBTU/HR	25 PPMV	GOOD COMBUSTION PRACTICES	0	BACT-PSD
AUBURNDALE POWER PARTNERS, LP	FL	Dec-92	TURBINE, GAS	1,214 MMBTU/HR	15 PPMV	GOOD COMBUSTION PRACTICES	0	BACT-PSD
SITHINDEPENDENCE POWER PARTNERS	NY	Nov-92	TURBINES, COMBUSTION (4) (NATURAL GAS) (1012 MW)	2,133 MMBTU/HR (EACH)	13 PPM	COMBUSTION CONTROLS	0	BACT-OTHER
KAMINE/BESICORP BEAVER FALLS COGENERATION FACILITY	NY	Nov-92	TURBINE, COMBUSTION (NAT. GAS & OIL FUEL) (79MW)	650 MMBTU/HR	9.5 PPM	COMBUSTION CONTROLS	0	BACT-OTHER
GRAY'S FERRY CO. GENERATION PARTNERSHIP	PA	Nov-92	TURBINE (NATURAL GAS & OIL)	1,150 MMBTU	0.0055 LBS/MMBTU (GAS)	COMBUSTION	0	BACT-OTHER
BEAR ISLAND PAPER COMPANY, L.P.	VA	Oct-92	TURBINE, COMBUSTION GAS	468 X10(8) BTU/HR #2 OIL	11 LBS/HR	GOOD COMBUSTION	0	BACT-PSD
BEAR ISLAND PAPER COMPANY, L.P.	VA	Oct-92	TURBINE, COMBUSTION GAS (TOTAL)	0	48 TYP	GOOD COMBUSTION	0	BACT-PSD

Table B-5. Summary of Best Available Control Technology (BACT) Determinations for Carbon Monoxide (CO) Emissions

Facility Name	State	Permit Issue Date	Unit/Process Description	Capacity (size)	CO Emission Limit	Control Method	Efficiency (%)	Type
BEAR ISLAND PAPER COMPANY, L.P.	VA	Oct-92	TURBINE, COMBUSTION GAS	474 X10(6) BTU/HR N. GAS	11 LBS/HR	GOOD COMBUSTION	0	BACT-PSD
PHILADELPHIA SOUTHWEST WATER TREATMENT PLANT	PA	Oct-92	ENGINES (2) (NATURAL GAS)	443 KW (EACH)	0	LEAN BURN ENGINE	0	OTHER
PHILADELPHIA NORTHEAST WATER TREATMENT PLANT	PA	Oct-92	ENGINES (2) (NATURAL GAS)	443 KW (EACH)	0	LEAN BURN ENGINE	0	OTHER
GORDONVILLE ENERGY L.P.	VA	Sep-92	TURBINE FACILITY, GAS	7.44 X10(7) GPM FUEL OIL	250 TOTAL TPY	GOOD COMBUSTION PRACTICES	0	BACT-PSD
GORDONVILLE ENERGY L.P.	VA	Sep-92	TURBINES (2) (EACH WITH A SF)	1.36 X10(9) BTU/H #2 OIL	66 LBS/HR/UNIT	GOOD COMBUSTION PRACTICES	0	BACT-PSD
GORDONVILLE ENERGY L.P.	VA	Sep-92	TURBINE FACILITY, GAS	1.331 X10(7) SCFY NAT GAS	250 TOTAL TPY	GOOD COMBUSTION PRACTICES	0	BACT-PSD
GORDONVILLE ENERGY L.P.	VA	Sep-92	TURBINES (2) (EACH WITH A SF)	1.51 X10(9) BTU/H N GAS	57 LBS/HR/UNIT	GOOD COMBUSTION PRACTICES	0	BACT-PSD
NEVADA POWER COMPANY, HARRY ALLEN PEAKING PLANT	NV	Sep-92	COMBUSTION TURBINE ELECTRIC POWER GENERATION	600 MW (8 UNITS 75 EACH)	153 TPY (EACH TURBINE)	PRECISION CONTROL FOR THE LOW NOX COMBUSTOR	0	BACT-PSD
KAMINE SOUTH OLENS FALLS COGEN CO	NY	Sep-92	GE FRAME 8 GAS TURBINE	406 MMBTU/HR	9 PPM, 11.0 LBS/HR	NO CONTROLS	0	BACT-OTHER
NORTHERN STATES POWER COMPANY	SD	Sep-92	TURBINE, SIMPLE CYCLE, 4 EACH	129 MW	50 PPM FOR GAS	GOOD COMBUSTION TECHNIQUES	0	BACT-PSD
PASNY/HOLTSVILLE COMBINED CYCLE PLANT	NY	Sep-92	TURBINE, COMBUSTION GAS (150 MW)	1,146 MMBTU/HR (GAS)*	8.5 PPM	COMBUSTION CONTROL	0	BACT-OTHER
WEPCU, PARIS SITE	VA	Aug-92	TURBINES, COMBUSTION (4)	0	25 LBS/HR (SEE NOTES)		0	BACT-PSD
FLORIDA POWER CORPORATION	FL	Aug-92	TURBINE, OIL	1,029 MMBTU/HR	54 LBS/H	GOOD COMBUSTION PRACTICES	0	BACT-PSD
FLORIDA POWER CORPORATION	FL	Aug-92	TURBINE, OIL	1,066 MMBTU/HR	79 LBS/H	GOOD COMBUSTION PRACTICES	0	BACT-PSD
CINC TRANSMISSION	OH	Aug-92	TURBINE (NATURAL GAS) (3)	5,500 HP (EACH)	0.015 GH/HR	FUEL SPEC: USE OF NATURAL GAS	0	BACT-PSD
SARAHAC ENERGY COMPANY	OH	Jul-92	TURBINES, COMBUSTION (2) (NATURAL GAS)	1,123 MMBTU/HR (EACH)	3 PPM	OXIDATION CATALYST	0	BACT-OTHER
HARTWELL ENERGY LIMITED PARTNERSHIP	GA	Jul-92	TURBINE, OIL FIRED (2 EACH)	1,840 MMBTU/HR	25 PPM @ 15% O2	FUEL SPEC: CLEAN BURNING FUELS	0	BACT-PSD
MAUI ELECTRIC COMPANY, LTD./AAALAA GENERATING STA	HI	Jul-92	TURBINE, COMBINED-CYCLE COMBUSTION	26 MW	27 LBS/HR	COMBUSTION TECHNOLOGY/DESIGN	0	BACT-OTHER
HARTWELL ENERGY LIMITED PARTNERSHIP	GA	Jul-92	TURBINE, GAS FIRED (2 EACH)	1,817 MMBTU/HR	25 PPM @ 15% O2	FUEL SPEC: CLEAN BURNING FUELS	0	BACT-PSD
INDECK-YERKES ENERGY SERVICES	NY	Jun-92	GE FRAME 8 GAS TURBINE (EP #00001)	432 MMBTU/HR	10 PPM, 10 LBS/HR	NO CONTROLS	0	BACT-OTHER
SELKIRK COGENERATION PARTNERS, L.P.	NY	Jun-92	COMBUSTION TURBINES (2) (252 MW)	1,173 MMBTU/HR (EACH)	10 PPM	COMBUSTION CONTROLS	0	BACT-OTHER
SELKIRK COGENERATION PARTNERS, L.P.	NY	Jun-92	COMBUSTION TURBINE (79 MW)	1,173 MMBTU/HR	25 PPM	COMBUSTION CONTROL	0	BACT-OTHER
TENASKA WASHINGTON PARTNERS, L.P.	VA	May-92	COGENERATION PLANT, COMBINED CYCLE	1.83 MMBTU/HR	20 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
NARRAGANSETT ELECTRIC/NEW ENGLAND POWER CO.	RI	Apr-92	TURBINE, GAS AND OIL BURNER	1,360 MMBTU/HR EACH	11 PPM @ 15% O2, GAS		0	BACT-PSD
KENTUCKY UTILITIES COMPANY	KY	Mar-92	TURBINE, #2 FUEL OIL/NATURAL GAS (8)	1,500 MM BTU/HR (EACH)	75 LBS/H (EACH)	COMBUSTION CONTROL	0	BACT-PSD
BERMUDA HUNDRED ENERGY LIMITED PARTNERSHIP	VA	Mar-92	TURBINE, COMBUSTION	1,176 MMBTU/HR NAT. GAS	62 LBS/HR/UNIT	FURNACE DESIGN	91	BACT-PSD
BERMUDA HUNDRED ENERGY LIMITED PARTNERSHIP	VA	Mar-92	TURBINE, COMBUSTION	1,117 MMBTU/HR NO2 FUEL OIL	62 LBS/HR/UNIT	FURNACE DESIGN	91	BACT-PSD
BERMUDA HUNDRED ENERGY LIMITED PARTNERSHIP	VA	Mar-92	TURBINE, COMBUSTION, 2	0	229 TYP/UNIT		0	BACT-PSD
THERMO INDUSTRIES, LTD.	CO	Feb-92	TURBINE, GAS FIRED, 5 EACH	246 MMBTU/HR	25 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
HAWAII ELECTRIC LIGHT CO., INC.	HI	Feb-92	TURBINE, FUEL OIL #2	20 MW	27 LBS/HR @ 100% PEAKLD	COMBUSTION DESIGN	0	BACT-PSD
HAWAII ELECTRIC LIGHT CO., INC.	HI	Feb-92	TURBINE, FUEL OIL #2	20 MW	56 LBS/H @ 75-100% PKLD	COMBUSTION DESIGN	0	BACT-PSD
HAWAII ELECTRIC LIGHT CO., INC.	HI	Feb-92	TURBINE, FUEL OIL #2	20 MW	181 LBS/H @ 50-75% PKLD	COMBUSTION DESIGN	0	BACT-PSD
HAWAII ELECTRIC LIGHT CO., INC.	HI	Feb-92	TURBINE, FUEL OIL #2	20 MW	478 LBS/H @ 25-50% PKLD	COMBUSTION DESIGN	0	BACT-PSD
SAVANNAH ELECTRIC AND POWER CO.	GA	Feb-92	TURBINES, 8	1,032 MMBTU/HR, NAT GAS	9 PPM @ 15% O2	FUEL SPEC: LOW SULFUR FUEL OIL	0	BACT-PSD
SAVANNAH ELECTRIC AND POWER CO.	GA	Feb-92	TURBINES, 8	972 MMBTU/HR, #2 OIL	9 PPM @ 15% O2	FUEL SPEC: LOW SULFUR FUEL OIL	0	BACT-PSD
KAMMERBERG/SICOPR NATURAL GAS LP	NY	Dec-91	GE FRAME 8 GAS TURBINE	500 MMBTU/HR	0.001 LBS/MBTU, 10 LBS/HR	NO CONTROLS	0	BACT-OTHER
DUKE POWER CO. LINCOLN COMBUSTION TURBINE STATION	NC	Dec-91	TURBINE, COMBUSTION	1,247 MM BTU/HR	60 LBS/HR	COMBUSTION CONTROL	0	BACT-PSD
DUKE POWER CO. LINCOLN COMBUSTION TURBINE STATION	NC	Dec-91	TURBINE, COMBUSTION	1,313 MM BTU/HR	59 LBS/HR	COMBUSTION CONTROL	0	BACT-PSD
MAUI ELECTRIC COMPANY, LTD.	HI	Dec-91	TURBINE, FUEL OIL #2	28 MW	0 SEE NOTES	GOOD COMBUSTION PRACTICES	0	BACT-PSD
KALAMAZOO POWER LIMITED	MI	Dec-91	TURBINE, GAS-FIRED, 2, W WASTE HEAT BOILERS	1,806 MMBTU/HR	20 PPMV	DRY LOW NOX TURBINES	0	BACT-PSD
LAKE COGEN LIMITED	FL	Nov-91	TURBINE, OIL, 2 EACH	42 MW	78 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
LAKE COGEN LIMITED	FL	Nov-91	TURBINE, GAS, 2 EACH	42 MW	42 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
ORLANDO UTILITIES COMMISSION	FL	Nov-91	TURBINE, GAS, 4 EACH	35 MW	10 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
ORLANDO UTILITIES COMMISSION	FL	Nov-91	TURBINE, OIL, 4 EACH	35 MW	10 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
SOUTHERN CALIFORNIA GAS	CA	Oct-91	TURBINE, GAS-FIRED	48 MMBTU/HR	7.74 PPM @ 15% O2	HIGH TEMPERATURE OXIDATION CATALYST	80	BACT-PSD
SOUTHERN CALIFORNIA GAS	CA	Oct-91	TURBINE, GAS FIRED, SOLAR MODEL H	5,500 HP	7.74 PPM @ 15% O2	HIGH TEMP OXIDATION CATALYST	80	BACT-PSD
EL PASO NATURAL GAS	AZ	Oct-91	TURBINE, GAS, SOLAR CENTAUR H	5,500 HP	10.5 PPM @ 15% O2	FUEL SPEC: LEAN FUEL MIX	0	BACT-PSD
EL PASO NATURAL GAS	AZ	Oct-91	TURBINE, GAS, SOLAR CENTAUR H	5,500 HP	10.5 PPM @ 15% O2	FUEL SPEC: LEAN FUEL MIX	0	BACT-PSD
FLORIDA POWER GENERATION	FL	Oct-91	TURBINE, OIL, 8 EACH	93 MW	54 LBS/H	COMBUSTION CONTROL	0	BACT-PSD
EL PASO NATURAL GAS	AZ	Oct-91	TURBINE, NAT. GAS TRANSM., GE FRAME 3	12,000 HP	60 PPM @ 15% O2	LEAN BURN	0	BACT-PSD
CAROLINA POWER AND LIGHT CO.	SC	Sep-91	TURBINE, I.C.	80 MW	60 LBS/H		0	BACT-PSD
ENRON LOUISIANA ENERGY COMPANY	LA	Aug-91	TURBINE, GAS, 2	39 MMBTU/HR	60 PPM @ 15% O2	BASE CASE, NO ADDITIONAL CONTROLS	0	BACT-PSD
ALGONQUIN GAS TRANSMISSION CO.	RI	Jul-91	TURBINE, GAS, 2	49 MMBTU/HR	0.114 LBS/MBTU	GOOD COMBUSTION PRACTICES	0	BACT-OTHER
CHARLES LARSEN POWER PLANT	FL	Jul-91	TURBINE, OIL, 1 EACH	80 MW	25 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
CHARLES LARSEN POWER PLANT	FL	Jul-91	TURBINE, GAS, 1 EACH	80 MW	25 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
SUNAS ENERGY INC.	VA	Jun-91	TURBINE, NATURAL GAS	98 MW	6 PPM @ 15% O2	CO CATALYST	80	BACT-PSD
SAGUARO POWER COMPANY	NV	Jun-91	COMBUSTION TURBINE GENERATOR	34.5 MW	9 PPM	CONVERTER (CATALYTIC)	90	BACT-PSD
FLORIDA POWER AND LIGHT	FL	Jun-91	TURBINE, OIL, 2 EACH	400 MW	33 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
FLORIDA POWER AND LIGHT	FL	Jun-91	TURBINE, GAS, 4 EACH	400 MW	30 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
FLORIDA POWER AND LIGHT	FL	Jun-91	TURBINE, CO, 4 EACH	400 MW	33 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
NORTHERN CONSOLIDATED POWER	PA	May-91	TURBINES, GAS, 2	34.6 KW EACH	110 T/YR	OXIDATION CATALYST	90	OTHER
LAKEWOOD COGENERATION, L.P.	NJ	Apr-91	TURBINES (#2 FUEL OIL) (2)	1,190 MMBTU/HR (EACH)	0.06 LBS/MBTU	TURBINE DESIGN	0	BACT-OTHER
LAKEWOOD COGENERATION, L.P.	NJ	Apr-91	TURBINES (NATURAL GAS) (2)	1,190 MMBTU/HR (EACH)	0.026 LBS/MBTU	TURBINE DESIGN	0	BACT-OTHER
CMARRON CHEMICAL	CO	Mar-91	TURBINE #2, GE FRAME 8	33 MW	250 T/YR, LESS THAN	CO CATALYST	0	OTHER
FLORIDA POWER AND LIGHT	FL	Mar-91	TURBINE, GAS, 4 EACH	240 MW	30 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
FLORIDA POWER AND LIGHT	FL	Mar-91	TURBINE, OIL, 4 EACH	0	33 PPM @ 15% O2	COMBUSTION CONTROL	0	BACT-PSD
NEVADA COGENERATION ASSOCIATES #2	NV	Jan-91	COMBINED-CYCLE POWER GENERATION	85 MW POWER OUTPUT	40 LBS/HR	CATALYTIC CONVERTER	0	BACT-PSD
NEVADA COGENERATION ASSOCIATES #1	NV	Jan-91	COMBINED-CYCLE POWER GENERATION	85 MW TOTAL OUTPUT	40 LBS/HR	CATALYTIC CONVERTER	0	BACT-PSD
NEWARK BAY COGENERATION PARTNERSHIP	NJ	Nov-90	TURBINE, NATURAL GAS FIRED	505 MMBTU/HR	0.055 LBS/MBTU	CATALYTIC OXIDATION	80	BACT-PSD
T&G COGEN COGENERATION PLANT	NY	Aug-90	GE LM2500 GAS TURBINE	215 MMBTU/HR	0.181 LBS/MBTU	CATALYTIC OXIDIZER	80	BACT
SC ELECTRIC AND GAS COMPANY - HAGOOD STATION	SC	Dec-89	INTERNAL COMBUSTION TURBINE	110 MEGAWATTS	73 LBS/HR	GOOD COMBUSTION PRACTICES	0	BACT-PSD
PEABODY MUNICIPAL LIGHT PLANT	MA	Nov-89	TURBINE, 38 MW NATURAL GAS FIRED	412 MMBTU/HR	40 PPM @ 15% O2	GOOD COMBUSTION PRACTICES	0	BACT-OTHER
MEGAN-RACINE ASSOCIATES, INC	NY	Aug-89	GE LM5000-N COMBINED CYCLE GAS TURBINE	401 LBS/MBTU	0.026 LBS/MBTU, 11 LBS/HR	NO CONTROLS	0	BACT-OTHER
UNOCAL	CA	Jul-89	TURBINE, GAS (SEE NOTES)	0	10 PPM @ 15% O2	OXIDATION CATALYST	75	BACT-OTHER

Note: PSD= Prevention of Significant Deterioration
 BACT= Best Available Control Technology
 LAER= Lowest Achievable Emission Rate

Table B-6. Direct and Indirect Capital Costs for CO Catalyst for Frame "F" Simple Cycle Operation

Cost Component	Costs	Basis of Cost Component
<u>Direct Capital Costs</u>		
CO Associated Equipment	\$235,000	Vendor Quote
Instrumentation	\$23,500	10% of SCR Associated Equipment
Sales Tax	\$14,100	6% of SCR Associated Equipment/Catalyst
Freight	\$47,965	5% of SCR Associated Equipment/Catalyst
Total Direct Capital Costs (TDCC)	\$320,565	
Recurring Capital Costs (RCC)	\$724,290	Catalyst; Vendor Based Estimate
TOTAL CAPITAL COSTS	\$1,044,855	Sum of TDCC, TDIC and RCC
<u>Direct Installation Costs</u>		
Foundation and supports	\$83,588	8% of Total Capital Costs; OAQPS Cost Control Manual
Handling & Erection	\$146,280	14% of Total Capital Costs; OAQPS Cost Control Manual
Electrical	\$41,794	4% of Total Capital Costs; OAQPS Cost Control Manual
Piping	\$20,897	2% of Total Capital Costs; OAQPS Cost Control Manual
Insulation for ductwork	\$10,449	1% of Total Capital Costs; OAQPS Cost Control Manual
Painting	\$10,449	1% of Total Capital Costs; OAQPS Cost Control Manual
Site Preparation	\$5,000	Engineering Estimate
Buildings	\$0	
Total Direct Installation Costs (TDIC)	\$318,456	
<u>Indirect Costs</u>		
Engineering	\$104,485	10% of Total Capital Costs; OAQPS Cost Control Manual
Construction and Field Expense	\$52,243	5% of Total Capital Costs; OAQPS Cost Control Manual
Contractor Fees	\$104,485	10% of Total Capital Costs; OAQPS Cost Control Manual
Start-up	\$20,897	2% of Total Capital Costs; OAQPS Cost Control Manual
Performance Tests	\$10,449	1% of Total Capital Costs; OAQPS Cost Control Manual
Allowance for Funds Used During Constructi	\$56,226	2.5% of Total Capital Costs; borrowed at a rate 7.0% for 9 months
Contingencies	\$31,346	3% of Total Capital Costs; OAQPS Cost Control Manual
TOTAL INDIRECT CAPITAL COST (TICC)	\$380,131	
TOTAL DIRECT and INDIRECT CAPITAL COSTS (TDICC)	\$1,743,442	Sum of TDCC, TDIC and TICC

Table B-7. Annualized Cost for CO Catalyst for Frame "F" Simple Cycle Operation

Cost Component	Cost	Basis of Cost Estimate
Direct Annual Costs		
Operating Personnel	\$8,320	8 hours/week at \$20/hr
Supervision	\$1,248	15% of Operating Personnel; OAQPS Cost Control Manual
Maintenance - Labor	\$4,368	0.5 hr per shift, \$24/hr; OAQPS Cost Manual
- Materials	\$4,368	100% of maintenance labor; OAQPS Cost Manual
Inventory Cost	\$26,509.02	Capital Recovery (11.74%) for 1/3 catalyst
Catalyst Disposal Cost	\$37,025	\$28/1,000 lb/hr mass flow over 3 years; developed from vendor quotes
Contingency	\$2,455	3% of direct costs
Total Direct Annual Costs (TDAC)	\$84,293	
Energy Costs		
Heat Rate Penalty	\$59,346	0.2% of MW output; EPA, 1993 (Page 6-20)
MW Loss Penalty	\$42,015	2 days replacement energy costs @ \$0.01 kWh each three period
Fuel Escalation	\$3,041	Escalation of fuel over inflation; 3% of energy costs
Contingency	\$3,132	3% of energy costs
Total Energy Costs (TEC)	\$107,533	
Indirect Annual Costs		
Overhead	\$8,362	60% of Operating/Supervision Labor and Ammonia
Property Taxes, insurance, admin.	\$69,738	4% of Total Capital Costs
Annualized Total Direct Capital	\$111,903	10.98% Capital Recovery Factor of 7% over 15 years times sum of TDCC, TDIC and TICC
Annualized Total Direct Recurring	\$276,027	38.11% Capital Recovery Factor of 7% over 3 years times RCC
Total Indirect Annual Costs (TIAC)	\$466,029	
TOTAL ANNUALIZED COSTS	\$657,856	Sum of TDAC, TEC and TIAC
COST EFFECTIVENESS	\$9,508	

APPENDIX C

BUILDING DOWNWASH INFORMATION FROM BPIP

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8/25/

'BPIP data for Sonat Power Project, Hardee County Site'

'ST'

'FEET' 0.3048

'UTMN' 0

12

'N.Demin.WTk' 1 0.0

8 50

400 200

364.6 185.4

350 150

364.6 114.6

400 100

435.4 114.6

450 150

435.4 185.4

'S.Demin.Wtk' 1 0.0

8 50

400 80

364.6 65.4

350 30

364.6 -5.4

400 -20

435.4 -5.4

450 30

435.4 65.4

'W.FO Tk' 1 0.0

8 50

256 -214

220.6 -228.6

206 -264

220.6 -299.4

256 -314

291.4 -299.4

306 -264

291.4 -228.6

'E.FO Tk' 1 0.0

8 50

400 -214

364.6 -228.6

350 -264

364.6 -299.4

400 -314

435.4 -299.4

450 -264

435.4 -228.6

'InlFilt1' 1 0.0

4 47

-94 104

-94 140

-58 140

-58 104

'InlFilt2' 1 0.0

4 47

22 104

22 140

58 140

58 104

'InlFilt3' 1 0.0

4 47

138 104

138 140

174 140

174 104

'InlFilt4' 1 0.0

4 47

254 104

254 140

290 140

290 104

'Turb1' 1 0.0

4 22.

-131 34

-131 76

-101 76

-101 34

'Turb2' 1 0.0

4 22.

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-15 34
-15 76
15 76
15 34
- 'Turb3' 1 0.0
4 22.
101 34
101 76
131 76
131 34
'Turb4' 1 0.0
4 22.
217 34
217 76
247 76
247 34
4
'CT1' 0.0 60 -116 0
'CT2' 0.0 60 0 0
'CT3' 0.0 60 116 0
'CT4' 0.0 60 232 0
0

BPIP (Dated: 95086)

DATE : 08/25/99

TIME : 11:27:35

BPIP data for Sonat Power Project, Hardee County Site

BPIP PROCESSING INFORMATION:

The ST flag has been set for processing for an ISCST2 run.

Inputs entered in FEET will be converted to meters using
a conversion factor of 0.3048. Output will be in meters.

UTMP is set to UTMN. The input is assumed to be in a local
X-Y coordinate system as opposed to a UTM coordinate system.
True North is in the positive Y direction.

Plant north is set to 0.00 degrees with respect to True North.

BPIP data for Sonat Power Project, Hardee County Site

PRELIMINARY* GEP STACK HEIGHT RESULTS TABLE
(Output Units: meters)

Stack Name	Stack Height	Stack-Building Base Elevation Differences	GEP** EQN1	Preliminary* GEP Stack Height Value
CT1	18.29	0.00	35.81	65.00
CT2	18.29	0.00	35.81	65.00
CT3	18.29	0.00	38.10	65.00
CT4	18.29	0.00	38.10	65.00

* Results are based on Determinants 1 & 2 on pages 1 & 2 of the GEP
Technical Support Document. Determinant 3 may be investigated for
additional stack height credit. Final values result after
Determinant 3 has been taken into consideration.

** Results were derived from Equation 1 on page 6 of GEP Technical
Support Document. Values have been adjusted for any stack-building
base elevation differences.

Note: Criteria for determining stack heights for modeling emission
limitations for a source can be found in Table 3.1 of the
GEP Technical Support Document.

BPIP (Dated: 95086)

DATE : 08/25/99

TIME : 11:27:35

BPIP data for Sonat Power Project, Hardee County Site

BPIP output is in meters

SO BUILDHGT CT1	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT CT1	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT CT1	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT CT1	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT CT1	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT CT1	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID CT1	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID CT1	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID CT1	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDWID CT1	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID CT1	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID CT1	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT CT2	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT CT2	0.00	0.00	0.00	6.71	6.71	6.71
SO BUILDHGT CT2	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT CT2	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT CT2	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT CT2	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID CT2	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID CT2	0.00	0.00	0.00	14.19	15.16	15.66
SO BUILDWID CT2	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID CT2	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID CT2	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID CT2	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT CT3	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT CT3	0.00	0.00	0.00	6.71	6.71	14.33
SO BUILDHGT CT3	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT CT3	14.33	14.33	14.33	14.33	15.24	15.24
SO BUILDHGT CT3	15.24	15.24	15.24	0.00	0.00	0.00
SO BUILDHGT CT3	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID CT3	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID CT3	0.00	0.00	0.00	14.19	15.16	14.99
SO BUILDWID CT3	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID CT3	12.71	14.06	14.99	15.46	58.42	61.15
SO BUILDWID CT3	28.64	30.02	30.48	0.00	0.00	0.00
SO BUILDWID CT3	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT CT4	15.24	6.71	15.24	15.24	15.24	0.00
SO BUILDHGT CT4	0.00	0.00	0.00	15.24	6.71	14.33
SO BUILDHGT CT4	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT CT4	14.33	14.33	15.24	15.24	15.24	15.24
SO BUILDHGT CT4	15.24	15.24	15.24	15.24	0.00	0.00
SO BUILDHGT CT4	0.00	15.24	15.24	15.24	15.24	15.24
SO BUILDWID CT4	30.02	12.97	47.77	53.91	58.42	0.00
SO BUILDWID CT4	0.00	0.00	0.00	66.04	15.16	14.99
SO BUILDWID CT4	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID CT4	12.71	14.06	29.48	30.40	30.40	29.48
SO BUILDWID CT4	28.64	30.02	30.48	30.02	0.00	0.00
SO BUILDWID CT4	0.00	64.02	67.49	28.64	30.02	30.48

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8/25/

BPIP (Dated: 95086)

DATE : 08/25/99

TIME : 11:27:35

BPIP data for Sonat Power Project, Hardee County Site

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BPIP PROCESSING INFORMATION:

=====

The ST flag has been set for processing for an ISCST2 run.

Inputs entered in FEET will be converted to meters using
a conversion factor of 0.3048. Output will be in meters.

UTMP is set to UTMN. The input is assumed to be in a local
X-Y coordinate system as opposed to a UTM coordinate system.
True North is in the positive Y direction.

Plant north is set to 0.00 degrees with respect to True North.

=====

INPUT SUMMARY:

=====

Number of buildings to be processed : 12

N.Demin has 1 tier(s) with a base elevation of 0.00 FEET
(0.00) meters

BUILDING NAME	TIER NUMBER	BLDG-TIER NUMBER	TIER HEIGHT	NO. OF CORNERS	CORNER X	COORDINATES Y
N.Demin	1	1	50.00 15.24 meters	8		
					400.00	200.00 FEET
					121.92	60.96 meters
					364.60	185.40 FEET
					111.13	56.51 meters
					350.00	150.00 FEET
					106.68	45.72 meters
					364.60	114.60 FEET
					111.13	34.93 meters
					400.00	100.00 FEET
					121.92	30.48 meters
					435.40	114.60 FEET
					132.71	34.93 meters
					450.00	150.00 FEET
					137.16	45.72 meters
					435.40	185.40 FEET
					132.71	56.51 meters

S.Demin has 1 tier(s) with a base elevation of 0.00 FEET
(0.00) meters

BUILDING NAME	TIER NUMBER	BLDG-TIER NUMBER	TIER HEIGHT	NO. OF CORNERS	CORNER X	COORDINATES Y
S.Demin	1	5	50.00 15.24 meters	8		
					400.00	80.00 FEET
					121.92	24.38 meters
					364.60	65.40 FEET
					111.13	19.93 meters
					350.00	30.00 FEET
					106.68	9.14 meters
					364.60	-5.40 FEET
					111.13	-1.65 meters
					400.00	-20.00 FEET
					121.92	-6.10 meters
					435.40	-5.40 FEET
					132.71	-1.65 meters

450.00	30.00 FEET
137.16	9.14 meters
435.40	65.40 FEET
132.71	19.93 meters

W.FO Tk has 1 tier(s) with a base elevation of 0.00 FEET
(0.00) meters

BUILDING NAME	TIER NUMBER	BLDG-TIER NUMBER	TIER HEIGHT	NO. OF CORNERS	CORNER X	COORDINATES Y
W.FO Tk	1	9	50.00 15.24 meters	8		

256.00	-214.00 FEET
78.03	-65.23 meters
220.60	-228.60 FEET
67.24	-69.68 meters
206.00	-264.00 FEET
62.79	-80.47 meters
220.60	-299.40 FEET
67.24	-91.26 meters
256.00	-314.00 FEET
78.03	-95.71 meters
291.40	-299.40 FEET
88.82	-91.26 meters
306.00	-264.00 FEET
93.27	-80.47 meters
291.40	-228.60 FEET
88.82	-69.68 meters

E.FO Tk has 1 tier(s) with a base elevation of 0.00 FEET
(0.00) meters

BUILDING NAME	TIER NUMBER	BLDG-TIER NUMBER	TIER HEIGHT	NO. OF CORNERS	CORNER X	COORDINATES Y
E.FO Tk	1	13	50.00 15.24 meters	8		

400.00	-214.00 FEET
121.92	-65.23 meters
364.60	-228.60 FEET
111.13	-69.68 meters
350.00	-264.00 FEET
106.68	-80.47 meters
364.60	-299.40 FEET
111.13	-91.26 meters
400.00	-314.00 FEET
121.92	-95.71 meters
435.40	-299.40 FEET
132.71	-91.26 meters
450.00	-264.00 FEET
137.16	-80.47 meters
435.40	-228.60 FEET
132.71	-69.68 meters

InlFilt1 has 1 tier(s) with a base elevation of 0.00 FEET
(0.00) meters

BUILDING NAME	TIER NUMBER	BLDG-TIER NUMBER	TIER HEIGHT	NO. OF CORNERS	CORNER X	COORDINATES Y
InlFilt1	1	17	47.00 14.33 meters	4		

-94.00	104.00 FEET
-28.65	31.70 meters
-94.00	140.00 FEET
-28.65	42.67 meters
-58.00	140.00 FEET
-17.68	42.67 meters
-58.00	104.00 FEET
-17.68	31.70 meters

InlFilt2 has 1 tier(s) with a base elevation of 0.00 FEET

(0.00) meters

BUILDING NAME	TIER NUMBER	BLDG-TIER NUMBER	TIER HEIGHT	NO. OF CORNERS	CORNER X	COORDINATES Y
InlFilt2	1	21	47.00	4		
			14.33 meters			
					22.00	104.00 FEET
					6.71	31.70 meters
					22.00	140.00 FEET
					6.71	42.67 meters
					58.00	140.00 FEET
					17.68	42.67 meters
					58.00	104.00 FEET
					17.68	31.70 meters

InlFilt3 has 1 tier(s) with a base elevation of 0.00 FEET
(0.00) meters

BUILDING NAME	TIER NUMBER	BLDG-TIER NUMBER	TIER HEIGHT	NO. OF CORNERS	CORNER X	COORDINATES Y
InlFilt3	1	25	47.00	4		
			14.33 meters			
					138.00	104.00 FEET
					42.06	31.70 meters
					138.00	140.00 FEET
					42.06	42.67 meters
					174.00	140.00 FEET
					53.04	42.67 meters
					174.00	104.00 FEET
					53.04	31.70 meters

InlFilt4 has 1 tier(s) with a base elevation of 0.00 FEET
(0.00) meters

BUILDING NAME	TIER NUMBER	BLDG-TIER NUMBER	TIER HEIGHT	NO. OF CORNERS	CORNER X	COORDINATES Y
InlFilt4	1	29	47.00	4		
			14.33 meters			
					254.00	104.00 FEET
					77.42	31.70 meters
					254.00	140.00 FEET
					77.42	42.67 meters
					290.00	140.00 FEET
					88.39	42.67 meters
					290.00	104.00 FEET
					88.39	31.70 meters

Turb1 has 1 tier(s) with a base elevation of 0.00 FEET
(0.00) meters

BUILDING NAME	TIER NUMBER	BLDG-TIER NUMBER	TIER HEIGHT	NO. OF CORNERS	CORNER X	COORDINATES Y
Turb1	1	33	22.00	4		
			6.71 meters			
					-131.00	34.00 FEET
					-39.93	10.36 meters
					-131.00	76.00 FEET
					-39.93	23.16 meters
					-101.00	76.00 FEET
					-30.78	23.16 meters
					-101.00	34.00 FEET
					-30.78	10.36 meters

Turb2 has 1 tier(s) with a base elevation of 0.00 FEET
(0.00) meters

BUILDING NAME	TIER NUMBER	BLDG-TIER NUMBER	TIER HEIGHT	NO. OF CORNERS	CORNER X	COORDINATES Y
---------------	-------------	------------------	-------------	----------------	----------	---------------

Turb2 1 37 22.00 4
6.71 meters

-15.00 34.00 FEET
-4.57 10.36 meters
-15.00 76.00 FEET
-4.57 23.16 meters
15.00 76.00 FEET
4.57 23.16 meters
15.00 34.00 FEET
4.57 10.36 meters

Turb3 has 1 tier(s) with a base elevation of 0.00 FEET
(0.00) meters

BUILDING NAME	TIER NUMBER	BLDG-TIER NUMBER	TIER HEIGHT	NO. OF CORNERS	CORNER X	COORDINATES Y
------------------	----------------	---------------------	----------------	-------------------	-------------	------------------

Turb3 1 41 22.00 4
6.71 meters

101.00 34.00 FEET
30.78 10.36 meters
101.00 76.00 FEET
30.78 23.16 meters
131.00 76.00 FEET
39.93 23.16 meters
131.00 34.00 FEET
39.93 10.36 meters

Turb4 has 1 tier(s) with a base elevation of 0.00 FEET
(0.00) meters

BUILDING NAME	TIER NUMBER	BLDG-TIER NUMBER	TIER HEIGHT	NO. OF CORNERS	CORNER X	COORDINATES Y
------------------	----------------	---------------------	----------------	-------------------	-------------	------------------

Turb4 1 45 22.00 4
6.71 meters

217.00 34.00 FEET
66.14 10.36 meters
217.00 76.00 FEET
66.14 23.16 meters
247.00 76.00 FEET
75.29 23.16 meters
247.00 34.00 FEET
75.29 10.36 meters

Number of stacks to be processed : 4

STACK NAME	STACK BASE	STACK HEIGHT	STACK X	COORDINATES Y
CT1	0.00	60.00 FEET		
(0.00	18.29) meters		
			-116.00	0.00 FEET
			-35.36	0.00) meters
CT2	0.00	60.00 FEET		
(0.00	18.29) meters		
			0.00	0.00 FEET
			0.00	0.00) meters
CT3	0.00	60.00 FEET		
(0.00	18.29) meters		
			116.00	0.00 FEET
			35.36	0.00) meters
CT4	0.00	60.00 FEET		
(0.00	18.29) meters		
			232.00	0.00 FEET
			70.71	0.00) meters

No stacks have been detected as being atop any structures.

Overall GEP Summary Table
(Units: meters)

StkNo: 1 Stk Name:CT1 Stk Ht: 18.29 Prelim. GEP Stk.Ht: 65.00

GEP: BH: 14.33 PBW: 14.34 *Eqn1 Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 1 Direction occurred: 202.50
 Bldg-Tier nos. contributing to GEP: 17

StkNo: 2 Stk Name:CT2 Stk Ht: 18.29 Prelim. GEP Stk.Ht: 65.00
 GEP: BH: 14.33 PBW: 14.34 *Eqn1 Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 1 Direction occurred: 202.50
 Bldg-Tier nos. contributing to GEP: 21

StkNo: 3 Stk Name:CT3 Stk Ht: 18.29 Prelim. GEP Stk.Ht: 65.00
 GEP: BH: 15.24 PBW: 29.76 *Eqn1 Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 1 Direction occurred: 257.50
 Bldg-Tier nos. contributing to GEP: 5

StkNo: 4 Stk Name:CT4 Stk Ht: 18.29 Prelim. GEP Stk.Ht: 65.00
 GEP: BH: 15.24 PBW: 28.20 *Eqn1 Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 1 Direction occurred: 247.50
 Bldg-Tier nos. contributing to GEP: 5

Summary By Direction Table
 (Units: meters)

Dominate stand alone tiers:

Drtcn: 10.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 11.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 11.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 11.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 30.02 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 3 Bld Name:W.FO Tk TierNo: 1

Drtcn: 20.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 12.97 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 12.97 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 12.97 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10

Single tier MAX: BH: 6.71 PBW: 12.97 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 12 Bld Name:Turb4 TierNo: 1

Drtcn: 30.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 14.32 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 14.32 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 14.32 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 14.32 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 12 Bld Name:Turb4 TierNo: 1

Drtcn: 40.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 5 Bld Name:InFilt1 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 6 Bld Name:InFilt2 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 7 Bld Name:InFilt3 TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 8 Bld Name:InFilt4 TierNo: 1

Drtcn: 50.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.

Drtcn: 60.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29

GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.

Drtcn: 70.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.

Drtcn: 80.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.

Drtcn: 90.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.

Drtcn: 100.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 14.19 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 14.19 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 14.19 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1

Drtcn: 110.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 15.16 *Wake Effect Ht: 16.76

*adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 15.16 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 15.16 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1

Drctn: 120.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 15.66 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 14.99 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 5 Bld Name:InlFilt1 TierNo: 1
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 14.99 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 6 Bld Name:InlFilt2 TierNo: 1

Drctn: 130.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 5 Bld Name:InlFilt1 TierNo: 1
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 6 Bld Name:InlFilt2 TierNo: 1
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 7 Bld Name:InlFilt3 TierNo: 1

Drctn: 140.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 15.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 5 Bld Name:InlFilt1 TierNo: 1
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 6 Bld Name:InlFilt2 TierNo: 1
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 7 Bld Name:InlFilt3 TierNo: 1

Drtcn: 150.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 14.32 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 14.99 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 5 Bld Name:InlFilt1 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 14.99 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 6 Bld Name:InlFilt2 TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 14.99 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 7 Bld Name:InlFilt3 TierNo: 1

Drtcn: 160.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 12.97 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 14.06 *Wake Effect Ht: 35.42
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 5 Bld Name:InlFilt1 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 14.06 *Wake Effect Ht: 35.42
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 6 Bld Name:InlFilt2 TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 14.06 *Wake Effect Ht: 35.42
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 7 Bld Name:InlFilt3 TierNo: 1

Drtcn: 170.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 11.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 11.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 11.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 11.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 12 Bld Name:Turb4 TierNo: 1

Drtcn: 180.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 9.14 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 9.14 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1

StkNo: -3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 9.14 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 9.14 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 12 Bld Name:Turb4 TierNo: 1

Drtcn: 190.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 12.71 *Wake Effect Ht: 33.39
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 5 Bld Name:InlFilt1 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 12.71 *Wake Effect Ht: 33.39
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 6 Bld Name:InlFilt2 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 12.71 *Wake Effect Ht: 33.39
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 7 Bld Name:InlFilt3 TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 12.71 *Wake Effect Ht: 33.39
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 8 Bld Name:InlFilt4 TierNo: 1

Drtcn: 200.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 14.06 *Wake Effect Ht: 35.42
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 5 Bld Name:InlFilt1 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 14.06 *Wake Effect Ht: 35.42
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 6 Bld Name:InlFilt2 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 14.06 *Wake Effect Ht: 35.42
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 7 Bld Name:InlFilt3 TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 14.06 *Wake Effect Ht: 35.42
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 8 Bld Name:InlFilt4 TierNo: 1

Drtcn: 210.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 14.99 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 5 Bld Name:InlFilt1 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 14.99 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 6 Bld Name:InlFilt2 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 14.99 *Wake Effect Ht: 35.81

*adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 7 Bld Name:InlFilt3 TierNo: 1
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 29.48 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 1 Bld Name:N.Demin TierNo: 1

Drtcn: 220.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 5 Bld Name:InlFilt1 TierNo: 1
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 6 Bld Name:InlFilt2 TierNo: 1
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 8 Bld Name:InlFilt4 TierNo: 1
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 30.40 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 1 Bld Name:N.Demin TierNo: 1

Drtcn: 230.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 6 Bld Name:InlFilt2 TierNo: 1
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 7 Bld Name:InlFilt3 TierNo: 1
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 15.46 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 8 Bld Name:InlFilt4 TierNo: 1
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 30.40 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 1 Bld Name:N.Demin TierNo: 1

Drtcn: 240.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 14.99 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 6 Bld Name:InlFilt2 TierNo: 1
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 14.33 PBW: 14.99 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 7 Bld Name:InlFilt3 TierNo: 1
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 14.33 PBW: 14.99 *Wake Effect Ht: 35.81
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 8 Bld Name:InlFilt4 TierNo: 1
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 29.48 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 2 Bld Name:S.Demin TierNo: 1

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Drtcn: 250.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 15.16 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 15.16 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 28.64 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 2 Bld Name:S.Demin TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 28.64 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 2 Bld Name:S.Demin TierNo: 1

Drtcn: 260.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 14.19 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 14.19 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 30.02 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 2 Bld Name:S.Demin TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 30.02 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 2 Bld Name:S.Demin TierNo: 1

Drtcn: 270.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 30.48 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 2 Bld Name:S.Demin TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 30.48 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 2 Bld Name:S.Demin TierNo: 1

Drtcn: 280.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29

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GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 30.02 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 2 Bld Name:S.Demin TierNo: 1

Drtcn: 290.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.

Drtcn: 300.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.

Drtcn: 310.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No single tier affects this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No single tier affects this stack for this direction.

Drtcn: 320.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 15.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 15.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 15.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 15.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 12 Bld Name:Turb4 TierNo: 1

Drtcn: 330.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81

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Single tier MAX: BH: 6.71 PBW: 14.32 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 14.32 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 14.32 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 14.32 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 12 Bld Name:Turb4 TierNo: 1

Drtcn: 340.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 12.97 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 12.97 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 12.97 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 28.64 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 3 Bld Name:W.FO Tk TierNo: 1

Drtcn: 350.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 11.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 11.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 11.23 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 30.02 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 3 Bld Name:W.FO Tk TierNo: 1

Drtcn: 360.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 9.14 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 9 Bld Name:Turb1 TierNo: 1

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 Single tier MAX: BH: 6.71 PBW: 9.14 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 10 Bld Name:Turb2 TierNo: 1

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 6.71 PBW: 9.14 *Wake Effect Ht: 16.76
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 11 Bld Name:Turb3 TierNo: 1
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Single tier MAX: BH: 15.24 PBW: 30.48 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 BldNo: 3 Bld Name:W.FO Tk TierNo: 1

Dominate combined buildings:

Drtcn: 10.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 73.24 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 9 13

Drtcn: 20.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 30.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 47.77 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

Drtcn: 40.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29

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GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 53.91 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

Drtn: 50.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 58.42 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

Drtn: 60.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtn: 70.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtn: 80.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtn: 90.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.

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StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 100.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 66.04 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

Drtcn: 110.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 120.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 130.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 140.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81

No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 150.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 160.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 170.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 180.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 190.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29

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8/25/95

GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 200.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 210.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 47.77 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

Drtcn: 220.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 53.91 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

Drtcn: 230.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 58.42 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 58.42 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

Drctn: 240.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 61.15 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 61.15 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

Drctn: 250.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 63.01 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 63.01 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

Drctn: 260.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 66.04 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 66.04 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

Drctn: 270.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.

StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.

StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 67.06 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2

Bldg-Tier nos. contributing to MAX: 1 5
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 67.06 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

Drtcn: 280.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 66.04 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 1 5

Drtcn: 290.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 300.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 310.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction

Drtcn: 320.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29

GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 64.02 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 9 13

Drtcn: 330.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 67.49 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 9 13

Drtcn: 340.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 69.89 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 9 13

Drtcn: 350.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.
 StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
 Combined tier MAX: BH: 15.24 PBW: 73.24 *Wake Effect Ht: 38.10
 *adjusted for a Stack-Building elevation difference of 0.00
 No. of Tiers affecting Stk: 2
 Bldg-Tier nos. contributing to MAX: 9 13

Drtcn: 360.00

StkNo: 1 Stk Name:CT1 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 2 Stk Name:CT2 Stack Ht: 18.29
 GEP: BH: 14.33 PBW: 14.34 *Equation 1 Ht: 35.81
 No combined tiers affect this stack for this direction.
 StkNo: 3 Stk Name:CT3 Stack Ht: 18.29
 GEP: BH: 15.24 PBW: 29.76 *Equation 1 Ht: 38.10
 No combined tiers affect this stack for this direction.

StkNo: 4 Stk Name:CT4 Stack Ht: 18.29
GEP: BH: 15.24 PBW: 28.20 *Equation 1 Ht: 38.10
Combined tier MAX: BH: 15.24 PBW: 74.37 *Wake Effect Ht: 38.10
*adjusted for a Stack-Building elevation difference of 0.00
No. of Tiers affecting Stk: 2
Bldg-Tier nos. contributing to MAX: 9 13

APPENDIX D

DETAILED SUMMARY OF ISCST MODEL RESULTS

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ISCB083 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :GENNG.087
 ISCST3 OUTPUT FILE NUMBER 2 :GENNG.088
 ISCST3 OUTPUT FILE NUMBER 3 :GENNG.089
 ISCST3 OUTPUT FILE NUMBER 4 :GENNG.090
 ISCST3 OUTPUT FILE NUMBER 5 :GENNG.091

First title for last output file is: 1987 SONAT HARDEE COUNTY SITE

8/25/99

Second title for last output file is: NATURAL GAS, GENERIC EMISSION RATES, 3 LOADS AND 2 TEMPERATURES

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
SOURCE GROUP ID: BASE32					
Annual	1987	0.01248	240.	15000.	87123124
	1988	0.01201	220.	15000.	88123124
	1989	0.01196	210.	300.	89123124
	1990	0.01546	250.	15000.	90123124
	1991	0.01383	240.	15000.	91123124
HIGH 24-Hour	1987	0.14978	80.	7000.	87040624
	1988	0.20047	220.	20000.	88091324
	1989	0.20101	180.	20000.	89012324
	1990	0.18980	230.	20000.	90011624
	1991	0.13692	250.	10000.	91040224
HIGH 8-Hour	1987	0.41303	60.	20000.	87120408
	1988	0.39232	240.	20000.	88011524
	1989	0.43457	180.	20000.	89012308
	1990	0.39739	180.	20000.	90041208
	1991	0.32688	240.	20000.	91122608
HIGH 3-Hour	1987	0.80207	110.	20000.	87031003
	1988	0.76167	220.	20000.	88091324
	1989	0.65842	350.	20000.	89060824
	1990	0.62848	250.	10000.	90041312
	1991	0.82723	70.	2000.	91051215
HIGH 1-Hour	1987	1.68787	90.	2000.	87082614
	1988	1.61233	20.	2000.	88082914
	1989	1.73693	310.	1500.	89070913
	1990	1.68193	30.	2000.	90042312
	1991	1.78281	290.	1500.	91083113
SOURCE GROUP ID: BASE95					
Annual	1987	0.01132	240.	15000.	87123124
	1988	0.01077	220.	15000.	88123124
	1989	0.01186	210.	300.	89123124
	1990	0.01392	250.	15000.	90123124
	1991	0.01259	240.	20000.	91123124
HIGH 24-Hour	1987	0.14448	80.	7000.	87040624
	1988	0.18685	220.	20000.	88091324
	1989	0.18691	180.	20000.	89012324
	1990	0.17532	230.	20000.	90011624
	1991	0.13984	270.	7000.	91061124
HIGH 8-Hour	1987	0.38152	60.	20000.	87120408
	1988	0.36398	240.	20000.	88011524
	1989	0.40189	180.	20000.	89012308
	1990	0.36705	180.	20000.	90041208
	1991	0.30586	70.	2000.	91051216
HIGH 3-Hour	1987	0.74421	110.	20000.	87031003
	1988	0.70506	220.	20000.	88091324
	1989	0.60876	350.	20000.	89060824
	1990	0.61963	250.	10000.	90041312
	1991	0.81515	70.	2000.	91051215
HIGH 1-Hour	1987	1.59669	60.	2000.	87061714
	1988	1.59151	20.	2000.	88082914
	1989	1.60114	250.	2000.	89082614
	1990	1.61887	30.	2000.	90092113
	1991	1.59840	270.	2000.	91061113
SOURCE GROUP ID: LD7532					

Annual	1987	0.01442	240.	15000.	87123124
	1988	0.01389	220.	15000.	88123124
	1989	0.01231	200.	15000.	89123124
	1990	0.01800	250.	15000.	90123124
	1991	0.01637	240.	15000.	91123124
HIGH 24-Hour	1987	0.17821	270.	10000.	87052424
	1988	0.22818	220.	15000.	88091324
	1989	0.22811	180.	20000.	89012324
	1990	0.21948	240.	15000.	90102724
	1991	0.16541	270.	10000.	91061124
HIGH 8-Hour	1987	0.47169	60.	20000.	87120408
	1988	0.43706	240.	20000.	88011524
	1989	0.49666	180.	20000.	89012308
	1990	0.45401	180.	20000.	90041208
	1991	0.37890	240.	20000.	91122608
HIGH 3-Hour	1987	0.90855	110.	20000.	87031003
	1988	0.86491	220.	20000.	88091324
	1989	0.74896	350.	20000.	89060824
	1990	0.97128	270.	2000.	90061315
	1991	0.84768	70.	2000.	91051215
HIGH 1-Hour	1987	2.10147	280.	1500.	87052413
	1988	1.95754	20.	1500.	88062313
	1989	2.01611	330.	1500.	89032712
	1990	2.08252	70.	1500.	90081414
	1991	2.10759	190.	1500.	91090612
SOURCE GROUP ID:	LD7595				
Annual	1987	0.01500	240.	15000.	87123124
	1988	0.01456	220.	15000.	88123124
	1989	0.01306	200.	15000.	89123124
	1990	0.01881	250.	12000.	90123124
	1991	0.01704	240.	15000.	91123124
HIGH 24-Hour	1987	0.18491	270.	10000.	87052424
	1988	0.23522	220.	15000.	88091324
	1989	0.24313	180.	20000.	89012324
	1990	0.22951	240.	15000.	90102724
	1991	0.17107	270.	10000.	91061124
HIGH 8-Hour	1987	0.49308	60.	20000.	87120408
	1988	0.43300	240.	20000.	88011524
	1989	0.51944	180.	20000.	89012308
	1990	0.47462	180.	20000.	90041208
	1991	0.39823	240.	20000.	91122608
HIGH 3-Hour	1987	0.94699	110.	20000.	87031003
	1988	0.90233	220.	20000.	88091324
	1989	0.78186	350.	20000.	89060824
	1990	0.97811	270.	2000.	90061315
	1991	0.85467	70.	2000.	91051215
HIGH 1-Hour	1987	2.15338	70.	1500.	87080713
	1988	2.12348	160.	1500.	88080712
	1989	2.18542	10.	1500.	89061912
	1990	2.16744	290.	1500.	90071012
	1991	2.17368	320.	1500.	91061514
SOURCE GROUP ID:	LD5032				
Annual	1987	0.01685	240.	15000.	87123124
	1988	0.01635	220.	15000.	88123124
	1989	0.01493	200.	15000.	89123124
	1990	0.02108	250.	12000.	90123124
	1991	0.01941	240.	15000.	91123124
HIGH 24-Hour	1987	0.20383	270.	10000.	87052424
	1988	0.24548	220.	20000.	88091324
	1989	0.27213	180.	15000.	89012324
	1990	0.25773	240.	15000.	90102724
	1991	0.17409	250.	10000.	91040224
HIGH 8-Hour	1987	0.55505	60.	15000.	87120408
	1988	0.50559	160.	1500.	88080716

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	1989	0.58108	180.	20000.	89012308
	1990	0.55770	160.	1500.	90061716
	1991	0.45136	240.	20000.	91122608
HIGH 3-Hour	1987	1.05883	110.	15000.	87031003
	1988	0.95051	220.	20000.	88091324
	1989	0.85828	350.	20000.	89060824
	1990	1.18045	40.	1500.	90042312
	1991	0.91606	270.	20000.	91010306
HIGH 1-Hour	1987	2.51939	250.	1500.	87082212
	1988	2.55232	360.	1500.	88081913
	1989	2.49256	180.	1500.	89041613
	1990	2.52849	60.	1500.	90072013
	1991	2.41349	330.	1500.	91040612
SOURCE GROUP ID: LD5095					
Annual	1987	0.01758	240.	15000.	87123124
	1988	0.01697	220.	15000.	88123124
	1989	0.01593	180.	15000.	89123124
	1990	0.02186	250.	12000.	90123124
	1991	0.02028	240.	15000.	91123124
HIGH 24-Hour	1987	0.20872	270.	10000.	87052424
	1988	0.24992	220.	20000.	88091324
	1989	0.28159	180.	15000.	89012324
	1990	0.26647	240.	15000.	90102724
	1991	0.21255	250.	5000.	91090224
HIGH 8-Hour	1987	0.57487	60.	15000.	87120408
	1988	0.50889	160.	1500.	88080716
	1989	0.60213	180.	15000.	89012308
	1990	0.56179	160.	1500.	90061716
	1991	0.46759	240.	20000.	91122608
HIGH 3-Hour	1987	1.09449	110.	15000.	87031003
	1988	0.95532	220.	20000.	88091324
	1989	0.87816	200.	15000.	89092106
	1990	1.18941	40.	1500.	90042312
	1991	0.94760	270.	20000.	91010306
HIGH 1-Hour	1987	2.53279	250.	1500.	87082212
	1988	2.56549	360.	1500.	88081913
	1989	2.50515	180.	1500.	89041613
	1990	2.54155	60.	1500.	90072013
	1991	2.42505	330.	1500.	91040612
All receptor computations reported with respect to a user-specified origin					
GRID	0.00	0.00			
DISCRETE	0.00	0.00			

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ISCBOB3 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :GENFO.087
 ISCST3 OUTPUT FILE NUMBER 2 :GENFO.088
 ISCST3 OUTPUT FILE NUMBER 3 :GENFO.089
 ISCST3 OUTPUT FILE NUMBER 4 :GENFO.090
 ISCST3-OUTPUT FILE NUMBER 5 :GENFO.091

First title for last output file is: 1987 SONAT HARDEE COUNTY SITE

8/14/99

Second title for last output file is: FUEL OIL, GENERIC EMISSION RATES, 3 LOADS AND 2 TEMPERATURES

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
SOURCE GROUP ID: BASE32					
Annual	1987	0.01217	240.	15000.	87123124
	1988	0.01173	220.	15000.	88123124
	1989	0.01194	210.	300.	89123124
	1990	0.01508	250.	15000.	90123124
	1991	0.01344	240.	15000.	91123124
HIGH 24-Hour	1987	0.14836	80.	7000.	87040624
	1988	0.19658	220.	20000.	88091324
	1989	0.19681	180.	20000.	89012324
	1990	0.18558	230.	20000.	90011624
	1991	0.13437	250.	10000.	91040224
HIGH 8-Hour	1987	0.40384	60.	20000.	87120408
	1988	0.38393	240.	20000.	88011524
	1989	0.42487	180.	20000.	89012308
	1990	0.38850	180.	20000.	90041208
	1991	0.31884	240.	20000.	91122608
HIGH 3-Hour	1987	0.78525	110.	20000.	87031003
	1988	0.74549	220.	20000.	88091324
	1989	0.64427	350.	20000.	89060824
	1990	0.62576	250.	10000.	90041312
	1991	0.82387	70.	2000.	91051215
HIGH 1-Hour	1987	1.68181	90.	2000.	87082614
	1988	1.60663	20.	2000.	88082914
	1989	1.73080	310.	1500.	89070913
	1990	1.67577	30.	2000.	90042312
	1991	1.61389	270.	2000.	91061113
SOURCE GROUP ID: BASE95					
Annual	1987	0.01276	240.	15000.	87123124
	1988	0.01224	220.	15000.	88123124
	1989	0.01199	210.	300.	89123124
	1990	0.01586	250.	15000.	90123124
	1991	0.01421	240.	15000.	91123124
HIGH 24-Hour	1987	0.15151	230.	7000.	87042724
	1988	0.20446	220.	20000.	88091324
	1989	0.20533	180.	20000.	89012324
	1990	0.19413	230.	20000.	90011624
	1991	0.14000	110.	7000.	91080924
HIGH 8-Hour	1987	0.42244	60.	20000.	87120408
	1988	0.40092	240.	20000.	88011524
	1989	0.44455	180.	20000.	89012308
	1990	0.40650	180.	20000.	90041208
	1991	0.33515	240.	20000.	91122608
HIGH 3-Hour	1987	0.81927	110.	20000.	87031003
	1988	0.77819	220.	20000.	88091324
	1989	0.67286	350.	20000.	89060824
	1990	0.95460	270.	2000.	90061315
	1991	0.83060	70.	2000.	91051215
HIGH 1-Hour	1987	1.78459	150.	1500.	87080813
	1988	1.61804	20.	2000.	88082914
	1989	1.74374	310.	1500.	89070913
	1990	1.83620	260.	1500.	90071613
	1991	1.78915	290.	1500.	91083113
SOURCE GROUP ID: LD7532					

Annual	1987	0.01430	240.	15000.	87123124
	1988	0.01375	220.	15000.	88123124
	1989	0.01222	200.	15000.	89123124
	1990	0.01792	250.	15000.	90123124
	1991	0.01624	240.	15000.	91123124
HIGH 24-Hour	1987	0.17756	270.	10000.	87052424
	1988	0.22716	220.	15000.	88091324
	1989	0.22714	180.	20000.	89012324
	1990	0.21852	240.	15000.	90102724
	1991	0.16488	270.	10000.	91061124
HIGH 8-Hour	1987	0.46962	60.	20000.	87120408
	1988	0.43517	240.	20000.	88011524
	1989	0.49446	180.	20000.	89012308
	1990	0.45201	180.	20000.	90041208
	1991	0.37704	240.	20000.	91122608
HIGH 3-Hour	1987	0.90480	110.	20000.	87031003
	1988	0.86125	220.	20000.	88091324
	1989	0.74574	350.	20000.	89060824
	1990	0.97060	270.	2000.	90061315
	1991	0.84698	70.	2000.	91051215
HIGH 1-Hour	1987	2.09999	280.	1500.	87052413
	1988	1.95593	20.	1500.	88062313
	1989	2.01453	330.	1500.	89032712
	1990	2.03440	200.	1500.	90081313
	1991	2.10609	190.	1500.	91090612
SOURCE GROUP ID: LD7595					
Annual	1987	0.01489	240.	15000.	87123124
	1988	0.01443	220.	15000.	88123124
	1989	0.01284	200.	15000.	89123124
	1990	0.01862	250.	12000.	90123124
	1991	0.01694	240.	15000.	91123124
HIGH 24-Hour	1987	0.18231	270.	10000.	87052424
	1988	0.23459	220.	15000.	88091324
	1989	0.23932	180.	20000.	89012324
	1990	0.22562	240.	15000.	90102724
	1991	0.16888	270.	10000.	91061124
HIGH 8-Hour	1987	0.48486	60.	20000.	87120408
	1988	0.42524	240.	20000.	88011524
	1989	0.51068	180.	20000.	89012308
	1990	0.46670	180.	20000.	90041208
	1991	0.39078	240.	20000.	91122608
HIGH 3-Hour	1987	0.93223	110.	20000.	87031003
	1988	0.88794	220.	20000.	88091324
	1989	0.76920	350.	20000.	89060824
	1990	0.97551	270.	2000.	90061315
	1991	0.85200	70.	2000.	91051215
HIGH 1-Hour	1987	2.12170	250.	1500.	87072411
	1988	1.96803	20.	1500.	88062313
	1989	2.15942	330.	1500.	89062212
	1990	2.16144	290.	1500.	90071012
	1991	2.16785	320.	1500.	91061514
SOURCE GROUP ID: LD5032					
Annual	1987	0.01650	240.	15000.	87123124
	1988	0.01593	220.	15000.	88123124
	1989	0.01455	200.	15000.	89123124
	1990	0.02072	250.	12000.	90123124
	1991	0.01886	240.	15000.	91123124
HIGH 24-Hour	1987	0.20498	250.	12000.	87112324
	1988	0.23990	220.	20000.	88091324
	1989	0.26568	180.	15000.	89012324
	1990	0.25168	240.	15000.	90102724
	1991	0.18430	270.	10000.	91061124
HIGH 8-Hour	1987	0.54122	60.	15000.	87120408
	1988	0.50337	160.	1500.	88080716

	1989	0.56822	180.	20000.	89012308
	1990	0.51858	180.	20000.	90041208
	1991	0.44014	240.	20000.	91122608
HIGH 3-Hour					
	1987	1.03387	110.	15000.	87031003
	1988	0.92741	220.	20000.	88091324
	1989	0.83886	350.	20000.	89060824
	1990	1.17424	40.	1500.	90042312
	1991	0.89392	270.	20000.	91010306
HIGH 1-Hour					
	1987	2.50980	250.	1500.	87082212
	1988	2.37943	260.	1500.	88040513
	1989	2.39547	30.	1500.	89062011
	1990	2.44629	120.	1500.	90080212
	1991	2.36298	130.	1500.	91092113
SOURCE GROUP ID: LD5095					
Annual					
	1987	0.01737	240.	15000.	87123124
	1988	0.01677	220.	15000.	88123124
	1989	0.01540	180.	15000.	89123124
	1990	0.02155	250.	12000.	90123124
	1991	0.02002	240.	15000.	91123124
HIGH 24-Hour					
	1987	0.20670	270.	10000.	87052424
	1988	0.24725	220.	20000.	88091324
	1989	0.27841	180.	15000.	89012324
	1990	0.26352	240.	15000.	90102724
	1991	0.21073	250.	5000.	91090224
HIGH 8-Hour					
	1987	0.56820	60.	15000.	87120408
	1988	0.50773	160.	1500.	88080716
	1989	0.59505	180.	15000.	89012308
	1990	0.56037	160.	1500.	90061716
	1991	0.46215	240.	20000.	91122608
HIGH 3-Hour					
	1987	1.08251	110.	15000.	87031003
	1988	0.94408	220.	20000.	88091324
	1989	0.86876	350.	20000.	89060824
	1990	1.18632	40.	1500.	90042312
	1991	0.93698	270.	20000.	91010306
HIGH 1-Hour					
	1987	2.52817	250.	1500.	87082212
	1988	2.56094	360.	1500.	88081913
	1989	2.50082	180.	1500.	89041613
	1990	2.53702	60.	1500.	90072013
	1991	2.42107	330.	1500.	91040612
All receptor computations reported with respect to a user-specified origin					
GRID	0.00	0.00			
DISCRETE	0.00	0.00			

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ISCB083 RELEASE 98056

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ISCST3 OUTPUT FILE NUMBER 1 : GENNGC1.087
ISCST3 OUTPUT FILE NUMBER 2 : GENNGC1.088
ISCST3 OUTPUT FILE NUMBER 3 : GENNGC1.089
ISCST3 OUTPUT FILE NUMBER 4 : GENNGC1.090
ISCST3 OUTPUT FILE NUMBER 5 : GENNGC1.091

First title for last output file is: 1987 SONAT HARDEE COUNTY SITE, AT PSD CLASS I AREA 8/25/99
Second title for last output file is: NATURAL GAS, GENERIC EMISSION RATES, 3 LOADS AND 2 TEMPERATURES

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)

SOURCE GROUP ID: BASE32					
Annual	1987	0.00111	340300.	3165700.	87123124
	1988	0.00187	340300.	3165700.	88123124
	1989	0.00256	340300.	3165700.	89123124
	1990	0.00156	340300.	3165700.	90123124
	1991	0.00106	340300.	3165700.	91123124
HIGH 24-Hour	1987	0.02971	340300.	3165700.	87122524
	1988	0.05210	340300.	3169800.	88122824
	1989	0.04930	340300.	3165700.	89042424
	1990	0.05073	340300.	3169800.	90021524
	1991	0.02766	340300.	3165700.	91042324
HIGH 8-Hour	1987	0.08875	343700.	3178300.	87011008
	1988	0.15630	340300.	3169800.	88122808
	1989	0.13451	340300.	3165700.	89071208
	1990	0.13741	340300.	3169800.	90021508
	1991	0.07951	340300.	3165700.	91042308
HIGH 3-Hour	1987	0.23345	340300.	3165700.	87041503
	1988	0.25106	340300.	3169800.	88040403
	1989	0.20683	340700.	3171900.	89111506
	1990	0.20232	340700.	3171900.	90021503
	1991	0.21135	340300.	3165700.	91042303
HIGH 1-Hour	1987	0.45487	340700.	3171900.	87090604
	1988	0.51196	340700.	3171900.	88080907
	1989	0.49547	340300.	3165700.	89071207
	1990	0.45532	340700.	3171900.	90112902
	1991	0.46254	340300.	3167700.	91042802
SOURCE GROUP ID: BASE95					
Annual	1987	0.00104	340300.	3165700.	87123124
	1988	0.00176	340300.	3165700.	88123124
	1989	0.00238	340300.	3165700.	89123124
	1990	0.00148	340300.	3165700.	90123124
	1991	0.00100	340300.	3165700.	91123124
HIGH 24-Hour	1987	0.02873	340300.	3165700.	87122524
	1988	0.04840	340300.	3169800.	88122824
	1989	0.04599	340300.	3165700.	89042424
	1990	0.04847	340300.	3169800.	90021524
	1991	0.02621	340300.	3165700.	91042324
HIGH 8-Hour	1987	0.08495	343700.	3178300.	87011008
	1988	0.14520	340300.	3169800.	88122808
	1989	0.12599	340300.	3165700.	89071208
	1990	0.13110	340300.	3169800.	90021508
	1991	0.07535	340300.	3165700.	91042308
HIGH 3-Hour	1987	0.22047	340300.	3165700.	87041503
	1988	0.24104	340300.	3169800.	88040403
	1989	0.19901	340700.	3171900.	89111506
	1990	0.19138	340700.	3171900.	90021503
	1991	0.20031	340300.	3165700.	91042303
HIGH 1-Hour	1987	0.43393	340700.	3171900.	87090604
	1988	0.48520	340700.	3171900.	88080907
	1989	0.46913	340300.	3165700.	89071207
	1990	0.43439	340700.	3171900.	90112902
	1991	0.44102	340300.	3167700.	91042802
SOURCE GROUP ID: LD7532					

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Annual	1987	0.00123	340300.	3165700.	87123124
	1988	0.00208	340300.	3165700.	88123124
	1989	0.00294	340300.	3165700.	89123124
	1990	0.00175	340300.	3165700.	90123124
	1991	0.00120	340300.	3165700.	91123124
HIGH 24-Hour	1987	0.03208	340300.	3165700.	87041524
	1988	0.05888	340300.	3169800.	88122824
	1989	0.05538	340300.	3165700.	89042424
	1990	0.05481	340300.	3169800.	90021524
	1991	0.03022	340300.	3165700.	91042324
HIGH 8-Hour	1987	0.09624	340300.	3165700.	87041508
	1988	0.17664	340300.	3169800.	88122808
	1989	0.14977	340300.	3165700.	89071208
	1990	0.14886	340300.	3169800.	90021508
	1991	0.08689	340300.	3165700.	91042308
HIGH 3-Hour	1987	0.25665	340300.	3165700.	87041503
	1988	0.26817	340300.	3169800.	88040403
	1989	0.22014	340700.	3171900.	89111506
	1990	0.22190	340700.	3171900.	90021503
	1991	0.23096	340300.	3165700.	91042303
HIGH 1-Hour	1987	0.49091	340700.	3171900.	87090604
	1988	0.55857	340700.	3171900.	88080907
	1989	0.54129	340300.	3165700.	89071207
	1990	0.49139	340700.	3171900.	90112902
	1991	0.49959	340300.	3167700.	91042802
SOURCE GROUP ID: LD7595					
Annual	1987	0.00126	340300.	3165700.	87123124
	1988	0.00216	340300.	3165700.	88123124
	1989	0.00304	340300.	3165700.	89123124
	1990	0.00182	340300.	3165700.	90123124
	1991	0.00123	340300.	3165700.	91123124
HIGH 24-Hour	1987	0.03311	340300.	3165700.	87041524
	1988	0.06132	340300.	3169800.	88122824
	1989	0.05757	340300.	3165700.	89042424
	1990	0.05619	340300.	3169800.	90021524
	1991	0.03113	340300.	3165700.	91042324
HIGH 8-Hour	1987	0.09984	342000.	3174000.	87073108
	1988	0.18397	340300.	3169800.	88122808
	1989	0.15524	340300.	3165700.	89071208
	1990	0.15274	340300.	3169800.	90021508
	1991	0.08950	340300.	3165700.	91042308
HIGH 3-Hour	1987	0.26490	340300.	3165700.	87041503
	1988	0.27402	340300.	3169800.	88040403
	1989	0.22468	340700.	3171900.	89111506
	1990	0.22883	340700.	3171900.	90021503
	1991	0.23788	340300.	3165700.	91042303
HIGH 1-Hour	1987	0.50335	340700.	3171900.	87090604
	1988	0.57482	340700.	3171900.	88080907
	1989	0.55729	340300.	3165700.	89071207
	1990	0.50384	340700.	3171900.	90112902
	1991	0.51239	340300.	3167700.	91042802
SOURCE GROUP ID: LD5032					
Annual	1987	0.00140	340300.	3165700.	87123124
	1988	0.00236	340300.	3165700.	88123124
	1989	0.00345	340300.	3165700.	89123124
	1990	0.00195	340300.	3165700.	90123124
	1991	0.00137	340300.	3165700.	91123124
HIGH 24-Hour	1987	0.03585	340300.	3165700.	87041524
	1988	0.06787	340300.	3169800.	88122824
	1989	0.06350	340300.	3165700.	89042424
	1990	0.05978	340300.	3169800.	90021524
	1991	0.03353	340300.	3165700.	91042324
HIGH 8-Hour	1987	0.11065	342000.	3174000.	87073108
	1988	0.20362	340300.	3169800.	88122808

	1989	0.16988	340300.	3165700.	89071208
	1990	0.16287	340300.	3169800.	90021508
	1991	0.09638	340300.	3165700.	91042308
HIGH 3-Hour	1987	0.28679	340300.	3165700.	87041503
	1988	0.30141	342000.	3174000.	88071103
	1989	0.23628	340700.	3171900.	89111506
	1990	0.24712	340700.	3171900.	90021503
	1991	0.25615	340300.	3165700.	91042303
HIGH 1-Hour	1987	0.53558	340700.	3171900.	87090604
	1988	0.61730	340700.	3171900.	88080907
	1989	0.59922	340300.	3165700.	89071207
	1990	0.53606	340700.	3171900.	90112902
	1991	0.54558	340300.	3167700.	91042802
SOURCE GROUP ID: LD5095					
Annual	1987	0.00143	340300.	3165700.	87123124
	1988	0.00242	340300.	3165700.	88123124
	1989	0.00352	340300.	3165700.	89123124
	1990	0.00201	340300.	3165700.	90123124
	1991	0.00139	340300.	3165700.	91123124
HIGH 24-Hour	1987	0.03665	340300.	3165700.	87041524
	1988	0.06981	340300.	3169800.	88122824
	1989	0.06526	340300.	3165700.	89042424
	1990	0.06083	340300.	3169800.	90021524
	1991	0.03422	340300.	3165700.	91042324
HIGH 8-Hour	1987	0.11382	342000.	3174000.	87073108
	1988	0.20943	340300.	3169800.	88122808
	1989	0.17414	340300.	3165700.	89071208
	1990	0.16582	340300.	3169800.	90021508
	1991	0.09838	340300.	3165700.	91042308
HIGH 3-Hour	1987	0.29316	340300.	3165700.	87041503
	1988	0.31153	342000.	3174000.	88071103
	1989	0.23953	340700.	3171900.	89111506
	1990	0.25245	340700.	3171900.	90021503
	1991	0.26145	340300.	3165700.	91042303
HIGH 1-Hour	1987	0.54469	340700.	3171900.	87090604
	1988	0.62940	340700.	3171900.	88080907
	1989	0.61115	340300.	3165700.	89071207
	1990	0.54518	340700.	3171900.	90112902
	1991	0.55497	340300.	3167700.	91042802

All receptor computations reported with respect to a user-specified origin

GRID	0.00	0.00
DISCRETE	0.00	0.00

ISCB083 RELEASE 98056

ISCST3 OUTPUT FILE NUMBER 1 :GENFOC1.087

ISCST3 OUTPUT FILE NUMBER 2 :GENFOC1.088

ISCST3 OUTPUT FILE NUMBER 3 :GENFOC1.089

ISCST3 OUTPUT FILE NUMBER 4 :GENFOC1.090

ISCST3 OUTPUT FILE NUMBER 5 :GENFOC1.091

First title for last output file is: 1987 SONAT HARDEE COUNTY SITE, AT PSD CLASS I AREA 8/25/99

Second title for last output file is: FUEL OIL, GENERIC EMISSION RATES, 3 LOADS AND 2 TEMPERATURES

AVERAGING TIME	YEAR	CONC (ug/m3)	DIR (deg) or X (m)	DIST (m) or Y (m)	PERIOD ENDING (YYMMDDHH)
SOURCE GROUP ID: BASE32					
Annual					
	1987	0.00109	340300.	3165700.	87123124
	1988	0.00183	340300.	3165700.	88123124
	1989	0.00251	340300.	3165700.	89123124
	1990	0.00153	340300.	3165700.	90123124
	1991	0.00105	340300.	3165700.	91123124
HIGH 24-Hour					
	1987	0.02943	340300.	3165700.	87122524
	1988	0.05103	340300.	3169800.	88122824
	1989	0.04835	340300.	3165700.	89042424
	1990	0.05009	340300.	3169800.	90021524
	1991	0.02724	340300.	3165700.	91042324
HIGH 8-Hour					
	1987	0.08766	343700.	3178300.	87011008
	1988	0.15309	340300.	3169800.	88122808
	1989	0.13209	340300.	3165700.	89071208
	1990	0.13561	340300.	3169800.	90021508
	1991	0.07832	340300.	3165700.	91042308
HIGH 3-Hour					
	1987	0.22974	340300.	3165700.	87041503
	1988	0.24822	340300.	3169800.	88040403
	1989	0.20463	340700.	3171900.	89111506
	1990	0.19917	340700.	3171900.	90021503
	1991	0.20820	340300.	3165700.	91042303
HIGH 1-Hour					
	1987	0.44897	340700.	3171900.	87090604
	1988	0.50440	340700.	3171900.	88080907
	1989	0.48805	340300.	3165700.	89071207
	1990	0.44941	340700.	3171900.	90112902
	1991	0.45648	340300.	3167700.	91042802
SOURCE GROUP ID: BASE95					
Annual					
	1987	0.00113	340300.	3165700.	87123124
	1988	0.00190	340300.	3165700.	88123124
	1989	0.00262	340300.	3165700.	89123124
	1990	0.00158	340300.	3165700.	90123124
	1991	0.00109	340300.	3165700.	91123124
HIGH 24-Hour					
	1987	0.02998	340300.	3165700.	87122524
	1988	0.05320	340300.	3169800.	88122824
	1989	0.05028	340300.	3165700.	89042424
	1990	0.05139	340300.	3169800.	90021524
	1991	0.02807	340300.	3165700.	91042324
HIGH 8-Hour					
	1987	0.08984	343700.	3178300.	87011008
	1988	0.15959	340300.	3169800.	88122808
	1989	0.13697	340300.	3165700.	89071208
	1990	0.13925	340300.	3169800.	90021508
	1991	0.08071	340300.	3165700.	91042308
HIGH 3-Hour					
	1987	0.23722	340300.	3165700.	87041503
	1988	0.25391	340300.	3169800.	88040403
	1989	0.20906	340700.	3171900.	89111506
	1990	0.20552	340700.	3171900.	90021503
	1991	0.21455	340300.	3165700.	91042303
HIGH 1-Hour					
	1987	0.46082	340700.	3171900.	87090604
	1988	0.51961	340700.	3171900.	88080907
	1989	0.50297	340300.	3165700.	89071207
	1990	0.46128	340700.	3171900.	90112902
	1991	0.46865	340300.	3167700.	91042802
SOURCE GROUP ID: LD7532					

Annual					
	1987	0.00122	340300.	3165700.	87123124
	1988	0.00207	340300.	3165700.	88123124
	1989	0.00290	340300.	3165700.	89123124
	1990	0.00175	340300.	3165700.	90123124
	1991	0.00120	340300.	3165700.	91123124
HIGH 24-Hour					
	1987	0.03198	340300.	3165700.	87041524
	1988	0.05864	340300.	3169800.	88122824
	1989	0.05516	340300.	3165700.	89042424
	1990	0.05467	340300.	3169800.	90021524
	1991	0.03013	340300.	3165700.	91042324
HIGH 8-Hour					
	1987	0.09594	340300.	3165700.	87041508
	1988	0.17593	340300.	3169800.	88122808
	1989	0.14924	340300.	3165700.	89071208
	1990	0.14847	340300.	3169800.	90021508
	1991	0.08664	340300.	3165700.	91042308
HIGH 3-Hour					
	1987	0.25584	340300.	3165700.	87041503
	1988	0.26759	340300.	3169800.	88040403
	1989	0.21969	340700.	3171900.	89111506
	1990	0.22122	340700.	3171900.	90021503
	1991	0.23028	340300.	3165700.	91042303
HIGH 1-Hour					
	1987	0.48967	340700.	3171900.	87090604
	1988	0.55697	340700.	3171900.	88080907
	1989	0.53971	340300.	3165700.	89071207
	1990	0.49016	340700.	3171900.	90112902
	1991	0.49832	340300.	3167700.	91042802
SOURCE GROUP ID: LD7595					
Annual					
	1987	0.00125	340300.	3165700.	87123124
	1988	0.00211	340300.	3165700.	88123124
	1989	0.00300	340300.	3165700.	89123124
	1990	0.00179	340300.	3165700.	90123124
	1991	0.00122	340300.	3165700.	91123124
HIGH 24-Hour					
	1987	0.03272	340300.	3165700.	87041524
	1988	0.06039	340300.	3169800.	88122824
	1989	0.05673	340300.	3165700.	89042424
	1990	0.05566	340300.	3169800.	90021524
	1991	0.03078	340300.	3165700.	91042324
HIGH 8-Hour					
	1987	0.09830	342000.	3174000.	87073108
	1988	0.18116	340300.	3169800.	88122808
	1989	0.15314	340300.	3165700.	89071208
	1990	0.15126	340300.	3169800.	90021508
	1991	0.08850	340300.	3165700.	91042308
HIGH 3-Hour					
	1987	0.26174	340300.	3165700.	87041503
	1988	0.27179	340300.	3169800.	88040403
	1989	0.22295	340700.	3171900.	89111506
	1990	0.22618	340700.	3171900.	90021503
	1991	0.23523	340300.	3165700.	91042303
HIGH 1-Hour					
	1987	0.49860	340700.	3171900.	87090604
	1988	0.56861	340700.	3171900.	88080907
	1989	0.55117	340300.	3165700.	89071207
	1990	0.49909	340700.	3171900.	90112902
	1991	0.50751	340300.	3167700.	91042802
SOURCE GROUP ID: LD5032					
Annual					
	1987	0.00137	340300.	3165700.	87123124
	1988	0.00232	340300.	3165700.	88123124
	1989	0.00340	340300.	3165700.	89123124
	1990	0.00193	340300.	3165700.	90123124
	1991	0.00133	340300.	3165700.	91123124
HIGH 24-Hour					
	1987	0.03528	340300.	3165700.	87041524
	1988	0.06650	340300.	3169800.	88122824
	1989	0.06226	340300.	3165700.	89042424
	1990	0.05904	340300.	3169800.	90021524
	1991	0.03303	340300.	3165700.	91042324
HIGH 8-Hour					
	1987	0.10837	342000.	3174000.	87073108
	1988	0.19951	340300.	3169800.	88122808

	1989	0.16680	340300.	3165700.	89071208
	1990	0.16078	340300.	3169800.	90021508
	1991	0.09496	340300.	3165700.	91042308
HIGH 3-Hour					
	1987	0.28222	340300.	3165700.	87041503
	1988	0.29417	342000.	3174000.	88071103
	1989	0.23391	340700.	3171900.	89111506
	1990	0.24333	340700.	3171900.	90021503
	1991	0.25236	340300.	3165700.	91042303
HIGH 1-Hour					
	1987	0.52894	340700.	3171900.	87090604
	1988	0.60850	340700.	3171900.	88080907
	1989	0.59051	340300.	3165700.	89071207
	1990	0.52943	340700.	3171900.	90112902
	1991	0.53874	340300.	3167700.	91042802
SOURCE GROUP ID: LD5095					
Annual					
	1987	0.00142	340300.	3165700.	87123124
	1988	0.00240	340300.	3165700.	88123124
	1989	0.00349	340300.	3165700.	89123124
	1990	0.00198	340300.	3165700.	90123124
	1991	0.00139	340300.	3165700.	91123124
HIGH 24-Hour					
	1987	0.03638	340300.	3165700.	87041524
	1988	0.06916	340300.	3169800.	88122824
	1989	0.06467	340300.	3165700.	89042424
	1990	0.06048	340300.	3169800.	90021524
	1991	0.03399	340300.	3165700.	91042324
HIGH 8-Hour					
	1987	0.11275	342000.	3174000.	87073108
	1988	0.20748	340300.	3169800.	88122808
	1989	0.17270	340300.	3165700.	89071208
	1990	0.16484	340300.	3169800.	90021508
	1991	0.09771	340300.	3165700.	91042308
HIGH 3-Hour					
	1987	0.29102	340300.	3165700.	87041503
	1988	0.30810	342000.	3174000.	88071103
	1989	0.23844	340700.	3171900.	89111506
	1990	0.25067	340700.	3171900.	90021503
	1991	0.25967	340300.	3165700.	91042303
HIGH 1-Hour					
	1987	0.54162	340700.	3171900.	87090604
	1988	0.62532	340700.	3171900.	88080907
	1989	0.60713	340300.	3165700.	89071207
	1990	0.54212	340700.	3171900.	90112902
	1991	0.55181	340300.	3167700.	91042802
All receptor computations reported with respect to a user-specified origin					
GRID	0.00	0.00			
DISCRETE	0.00	0.00			

CO STARTING
 CO TITLEONE 1987 SONAT HARDEE COUNTY SITE 8/25/99
 CO TITLETWO NATURAL GAS, GENERIC EMISSION RATES, 3 LOADS AND 2 TEMPERATURES
 CO MODELOPT DFAULT CONC RURAL NOCMPL
 CO AVERTIME PERIOD 24 8 3 1
 CO POLLUTID GEN
 CO DCAYCOEF .000000
 CO RUNORNOT RUN
 CO FINISHED

SO STARTING

** Source Location Cards:

** SRCID SRCTYP XS YS ZS

** MODELING ORIGIN CT 3 STACK LOCATION

** LOCATION IS USED FOR POLAR DISCRETE RECEPTORS.

** CT STACK NUMBER CODE

** -----

** B - CT 1

** C - CT 2

** D - CT 3

** E - CT 4

** Source Location Cards:

** SRCID	SRCTYP	XS (m)	YS (m)	ZS (m)
SO LOCATION	BASE32A POINT	-35.36	0.0	0.0
SO LOCATION	BASE32B POINT	0.00	0.0	0.0
SO LOCATION	BASE32C POINT	35.36	0.0	0.0
SO LOCATION	BASE32D POINT	70.71	0.0	0.0
SO LOCATION	BASE95A POINT	-35.36	0.0	0.0
SO LOCATION	BASE95B POINT	0.00	0.0	0.0
SO LOCATION	BASE95C POINT	35.36	0.0	0.0
SO LOCATION	BASE95D POINT	70.71	0.0	0.0
SO LOCATION	LD7532A POINT	-35.36	0.0	0.0
SO LOCATION	LD7532B POINT	0.00	0.0	0.0
SO LOCATION	LD7532C POINT	35.36	0.0	0.0
SO LOCATION	LD7532D POINT	70.71	0.0	0.0
SO LOCATION	LD7595A POINT	-35.36	0.0	0.0
SO LOCATION	LD7595B POINT	0.00	0.0	0.0
SO LOCATION	LD7595C POINT	35.36	0.0	0.0
SO LOCATION	LD7595D POINT	70.71	0.0	0.0
SO LOCATION	LD5032A POINT	-35.36	0.0	0.0
SO LOCATION	LD5032B POINT	0.00	0.0	0.0
SO LOCATION	LD5032C POINT	35.36	0.0	0.0
SO LOCATION	LD5032D POINT	70.71	0.0	0.0
SO LOCATION	LD5095A POINT	-35.36	0.0	0.0
SO LOCATION	LD5095B POINT	0.00	0.0	0.0
SO LOCATION	LD5095C POINT	35.36	0.0	0.0
SO LOCATION	LD5095D POINT	70.71	0.0	0.0

** Source Parameter Cards:

** SRCID	QS (g/s)	HS (m)	TS (K)	VS (m/s)	DS (m)
SO SRCPARAM	BASE32A	2.5000	18.3	864.8	36.18
SO SRCPARAM	BASE32B	2.5000	18.3	864.8	36.18
SO SRCPARAM	BASE32C	2.5000	18.3	864.8	36.18
SO SRCPARAM	BASE32D	2.5000	18.3	864.8	36.18
SO SRCPARAM	BASE95A	2.5000	18.3	885.9	38.86
SO SRCPARAM	BASE95B	2.5000	18.3	885.9	38.86
SO SRCPARAM	BASE95C	2.5000	18.3	885.9	38.86
SO SRCPARAM	BASE95D	2.5000	18.3	885.9	38.86
SO SRCPARAM	LD7532A	2.5000	18.3	905.4	30.63
SO SRCPARAM	LD7532B	2.5000	18.3	905.4	30.63
SO SRCPARAM	LD7532C	2.5000	18.3	905.4	30.63
SO SRCPARAM	LD7532D	2.5000	18.3	905.4	30.63
SO SRCPARAM	LD7595A	2.5000	18.3	918.2	28.96
SO SRCPARAM	LD7595B	2.5000	18.3	918.2	28.96
SO SRCPARAM	LD7595C	2.5000	18.3	918.2	28.96
SO SRCPARAM	LD7595D	2.5000	18.3	918.2	28.96
SO SRCPARAM	LD5032A	2.5000	18.3	905.9	25.66
SO SRCPARAM	LD5032B	2.5000	18.3	905.9	25.66
SO SRCPARAM	LD5032C	2.5000	18.3	905.9	25.66
SO SRCPARAM	LD5032D	2.5000	18.3	905.9	25.66
SO SRCPARAM	LD5095A	2.5000	18.3	922.0	24.54
SO SRCPARAM	LD5095B	2.5000	18.3	922.0	24.54
SO SRCPARAM	LD5095C	2.5000	18.3	922.0	24.54
SO SRCPARAM	LD5095D	2.5000	18.3	922.0	24.54

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D:\PROJECTS\SONAT\LOAD\GENNG.187

8/25/

SO BUILDHGT	BASE32A-BASE95A	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	BASE32A-BASE95A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32A-BASE95A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32A-BASE95A	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32A-BASE95A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32A-BASE95A	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	BASE32A-BASE95A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32A-BASE95A	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDWID	BASE32A-BASE95A	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	BASE32A-BASE95A	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32A-BASE95A	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDHGT	LD5032A-LD7595A	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	LD5032A-LD7595A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032A-LD7595A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	LD5032A-LD7595A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032A-LD7595A	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032A-LD7595A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032A-LD7595A	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	LD5032A-LD7595A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032A-LD7595A	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDWID	LD5032A-LD7595A	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	LD5032A-LD7595A	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032A-LD7595A	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT	BASE32B-BASE95B	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	BASE32B-BASE95B	0.00	0.00	0.00	6.71	6.71	6.71
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32B-BASE95B	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32B-BASE95B	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32B-BASE95B	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	BASE32B-BASE95B	0.00	0.00	0.00	14.19	15.16	15.66
SO BUILDWID	BASE32B-BASE95B	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	BASE32B-BASE95B	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	BASE32B-BASE95B	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32B-BASE95B	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDHGT	LD5032B-LD7595B	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	LD5032B-LD7595B	0.00	0.00	0.00	6.71	6.71	6.71
SO BUILDHGT	LD5032B-LD7595B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032B-LD7595B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032B-LD7595B	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032B-LD7595B	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032B-LD7595B	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	LD5032B-LD7595B	0.00	0.00	0.00	14.19	15.16	15.66
SO BUILDWID	LD5032B-LD7595B	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	LD5032B-LD7595B	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	LD5032B-LD7595B	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032B-LD7595B	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT	BASE32C-BASE95C	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	0.00	0.00	6.71	6.71	14.33
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	15.24	15.24
SO BUILDHGT	BASE32C-BASE95C	15.24	15.24	15.24	0.00	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32C-BASE95C	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	0.00	0.00	14.19	15.16	14.99
SO BUILDWID	BASE32C-BASE95C	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	BASE32C-BASE95C	12.71	14.06	14.99	15.46	58.42	61.15
SO BUILDWID	BASE32C-BASE95C	28.64	30.02	30.48	0.00	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDHGT	LD5032C-LD7595C	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	LD5032C-LD7595C	0.00	0.00	0.00	6.71	6.71	14.33
SO BUILDHGT	LD5032C-LD7595C	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032C-LD7595C	14.33	14.33	14.33	14.33	15.24	15.24
SO BUILDHGT	LD5032C-LD7595C	15.24	15.24	15.24	0.00	0.00	0.00
SO BUILDHGT	LD5032C-LD7595C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032C-LD7595C	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	LD5032C-LD7595C	0.00	0.00	0.00	14.19	15.16	14.99
SO BUILDWID	LD5032C-LD7595C	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	LD5032C-LD7595C	12.71	14.06	14.99	15.46	58.42	61.15
SO BUILDWID	LD5032C-LD7595C	28.64	30.02	30.48	0.00	0.00	0.00
SO BUILDWID	LD5032C-LD7595C	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT	BASE32D-BASE95D	15.24	6.71	15.24	15.24	15.24	0.00
SO BUILDHGT	BASE32D-BASE95D	0.00	0.00	0.00	15.24	6.71	14.33
SO BUILDHGT	BASE32D-BASE95D	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32D-BASE95D	14.33	14.33	15.24	15.24	15.24	15.24
SO BUILDHGT	BASE32D-BASE95D	15.24	15.24	15.24	15.24	0.00	0.00
SO BUILDHGT	BASE32D-BASE95D	0.00	15.24	15.24	15.24	15.24	15.24
SO BUILDWID	BASE32D-BASE95D	30.02	12.97	47.77	53.91	58.42	0.00
SO BUILDWID	BASE32D-BASE95D	0.00	0.00	0.00	66.04	15.16	14.99
SO BUILDWID	BASE32D-BASE95D	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	BASE32D-BASE95D	12.71	14.06	29.48	30.40	30.40	29.48
SO BUILDWID	BASE32D-BASE95D	28.64	30.02	30.48	30.02	0.00	0.00
SO BUILDWID	BASE32D-BASE95D	0.00	64.02	67.49	28.64	30.02	30.48
SO BUILDHGT	LD5032D-LD7595D	15.24	6.71	15.24	15.24	15.24	0.00
SO BUILDHGT	LD5032D-LD7595D	0.00	0.00	0.00	15.24	6.71	14.33
SO BUILDHGT	LD5032D-LD7595D	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032D-LD7595D	14.33	14.33	15.24	15.24	15.24	15.24
SO BUILDHGT	LD5032D-LD7595D	15.24	15.24	15.24	15.24	0.00	0.00
SO BUILDHGT	LD5032D-LD7595D	0.00	15.24	15.24	15.24	15.24	15.24
SO BUILDWID	LD5032D-LD7595D	30.02	12.97	47.77	53.91	58.42	0.00
SO BUILDWID	LD5032D-LD7595D	0.00	0.00	0.00	66.04	15.16	14.99
SO BUILDWID	LD5032D-LD7595D	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	LD5032D-LD7595D	12.71	14.06	29.48	30.40	30.40	29.48
SO BUILDWID	LD5032D-LD7595D	28.64	30.02	30.48	30.02	0.00	0.00
SO BUILDWID	LD5032D-LD7595D	0.00	64.02	67.49	28.64	30.02	30.48

SO EMISUNIT .100000E+07 (GRAMS/SEC) (MICROGRAMS/CUBIC-METER)

SO SRCGROUP BASE32 BASE32A BASE32B BASE32C BASE32D

SO SRCGROUP BASE95 BASE95A BASE95B BASE95C BASE95D

SO SRCGROUP LD7532 LD7532A LD7532B LD7532C LD7532D

SO SRCGROUP LD7595 LD7595A LD7595B LD7595C LD7595D

SO SRCGROUP LD5032 LD5032A LD5032B LD5032C LD5032D

SO SRCGROUP LD5095 LD5095A LD5095B LD5095C LD5095D

SO FINISHED

RE STARTING

RE GRIDPOLR POL STA

RE GRIDPOLR POL ORIG 0.0 0.0

RE GRIDPOLR POL DIST 100 200 300 500 700 1000 1500 2000 2500 3000 4000 5000

RE GRIDPOLR POL DIST 7000 10000 12000 15000 20000 25000 30000

RE GRIDPOLR POL GDIR 36 10.00 10.00

RE GRIDPOLR POL END

RE FINISHED

ME STARTING

ME INPUTFIL D:\MET\TPAPRL87.BIN UNIFORM

ME ANEMHGT 6.700 METERS

ME SURFDATA 12842 1987 TAMPA

ME UAIRDATA 12842 1987 RUSKIN

ME WINDCATS 1.54 3.09 5.14 8.23 10.80

ME FINISHED

OU STARTING

OU RECTABLE ALLAVE FIRST

OU FINISHED

CO STARTING
 CO TITLEONE 1987 SONAT HARDEE COUNTY SITE 8/14/99
 CO TITLETWO FUEL OIL, GENERIC EMISSION RATES, 3 LOADS AND 2 TEMPERATURES
 CO MODELOPT DFAULT CONC RURAL NOCMPL
 CO AVERTIME PERIOD 24 8 3 1
 CO POLLUTID GEN
 CO DCAYCOEF .000000
 CO RUNORNOT RUN
 CO FINISHED

SO STARTING

** Source Location Cards:

** SRCID SRCTYP XS YS ZS
 ** MODELING ORIGIN CT 3 STACK LOCATION
 ** LOCATION IS USED FOR POLAR DISCRETE RECEPTORS.
 ** CT STACK NUMBER CODE

** B - CT 1
 ** C - CT 2
 ** D - CT 3
 ** E - CT 4

** Source Location Cards:

** SRCID	** SRCTYP	XS (m)	YS (m)	ZS (m)
SO LOCATION	BASE32A POINT	-35.36	0.0	0.0
SO LOCATION	BASE32B POINT	0.00	0.0	0.0
SO LOCATION	BASE32C POINT	35.36	0.0	0.0
SO LOCATION	BASE32D POINT	70.71	0.0	0.0
SO LOCATION	BASE95A POINT	-35.36	0.0	0.0
SO LOCATION	BASE95B POINT	0.00	0.0	0.0
SO LOCATION	BASE95C POINT	35.36	0.0	0.0
SO LOCATION	BASE95D POINT	70.71	0.0	0.0
SO LOCATION	LD7532A POINT	-35.36	0.0	0.0
SO LOCATION	LD7532B POINT	0.00	0.0	0.0
SO LOCATION	LD7532C POINT	35.36	0.0	0.0
SO LOCATION	LD7532D POINT	70.71	0.0	0.0
SO LOCATION	LD7595A POINT	-35.36	0.0	0.0
SO LOCATION	LD7595B POINT	0.00	0.0	0.0
SO LOCATION	LD7595C POINT	35.36	0.0	0.0
SO LOCATION	LD7595D POINT	70.71	0.0	0.0
SO LOCATION	LD5032A POINT	-35.36	0.0	0.0
SO LOCATION	LD5032B POINT	0.00	0.0	0.0
SO LOCATION	LD5032C POINT	35.36	0.0	0.0
SO LOCATION	LD5032D POINT	70.71	0.0	0.0
SO LOCATION	LD5095A POINT	-35.36	0.0	0.0
SO LOCATION	LD5095B POINT	0.00	0.0	0.0
SO LOCATION	LD5095C POINT	35.36	0.0	0.0
SO LOCATION	LD5095D POINT	70.71	0.0	0.0

** Source Parameter Cards:

** POINT:	SRCID	QS (g/s)	HS (m)	TS (K)	VS (m/s)	DS (m)
SO SRCPARAM	BASE32A	2.500	18.3	853.2	37.31	6.71
SO SRCPARAM	BASE32B	2.500	18.3	853.2	37.31	6.71
SO SRCPARAM	BASE32C	2.500	18.3	853.2	37.31	6.71
SO SRCPARAM	BASE32D	2.500	18.3	853.2	37.31	6.71
SO SRCPARAM	BASE95A	2.500	18.3	878.2	35.05	6.71
SO SRCPARAM	BASE95B	2.500	18.3	878.2	35.05	6.71
SO SRCPARAM	BASE95C	2.500	18.3	878.2	35.05	6.71
SO SRCPARAM	BASE95D	2.500	18.3	878.2	35.05	6.71
SO SRCPARAM	LD7532A	2.500	18.3	905.4	30.78	6.71
SO SRCPARAM	LD7532B	2.500	18.3	905.4	30.78	6.71
SO SRCPARAM	LD7532C	2.500	18.3	905.4	30.78	6.71
SO SRCPARAM	LD7532D	2.500	18.3	905.4	30.78	6.71
SO SRCPARAM	LD7595A	2.500	18.3	914.3	29.57	6.71
SO SRCPARAM	LD7595B	2.500	18.3	914.3	29.57	6.71
SO SRCPARAM	LD7595C	2.500	18.3	914.3	29.57	6.71
SO SRCPARAM	LD7595D	2.500	18.3	914.3	29.57	6.71
SO SRCPARAM	LD5032A	2.500	18.3	922.0	26.12	6.71
SO SRCPARAM	LD5032B	2.500	18.3	922.0	26.12	6.71
SO SRCPARAM	LD5032C	2.500	18.3	922.0	26.12	6.71
SO SRCPARAM	LD5032D	2.500	18.3	922.0	26.12	6.71
SO SRCPARAM	LD5095A	2.500	18.3	922.0	24.84	6.71
SO SRCPARAM	LD5095B	2.500	18.3	922.0	24.84	6.71
SO SRCPARAM	LD5095C	2.500	18.3	922.0	24.84	6.71
SO SRCPARAM	LD5095D	2.500	18.3	922.0	24.84	6.71

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D:\PROJECTS\SONAT\LOAD\GENFO.187

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SO BUILDHGT	BASE32A-BASE95A	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	BASE32A-BASE95A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32A-BASE95A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32A-BASE95A	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32A-BASE95A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32A-BASE95A	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	BASE32A-BASE95A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32A-BASE95A	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDWID	BASE32A-BASE95A	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	BASE32A-BASE95A	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32A-BASE95A	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDHGT	LD5032A-LD7595A	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	LD5032A-LD7595A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032A-LD7595A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	LD5032A-LD7595A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032A-LD7595A	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032A-LD7595A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032A-LD7595A	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	LD5032A-LD7595A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032A-LD7595A	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDWID	LD5032A-LD7595A	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	LD5032A-LD7595A	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032A-LD7595A	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT	BASE32B-BASE95B	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	BASE32B-BASE95B	0.00	0.00	0.00	6.71	6.71	6.71
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32B-BASE95B	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32B-BASE95B	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32B-BASE95B	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	BASE32B-BASE95B	0.00	0.00	0.00	14.19	15.16	15.66
SO BUILDWID	BASE32B-BASE95B	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	BASE32B-BASE95B	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	BASE32B-BASE95B	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32B-BASE95B	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDHGT	LD5032B-LD7595B	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	LD5032B-LD7595B	0.00	0.00	0.00	6.71	6.71	6.71
SO BUILDHGT	LD5032B-LD7595B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032B-LD7595B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032B-LD7595B	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032B-LD7595B	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032B-LD7595B	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	LD5032B-LD7595B	0.00	0.00	0.00	14.19	15.16	15.66
SO BUILDWID	LD5032B-LD7595B	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	LD5032B-LD7595B	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	LD5032B-LD7595B	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032B-LD7595B	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT	BASE32C-BASE95C	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	0.00	0.00	6.71	6.71	14.33
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	15.24	15.24
SO BUILDHGT	BASE32C-BASE95C	15.24	15.24	15.24	0.00	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32C-BASE95C	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	0.00	0.00	14.19	15.16	14.99
SO BUILDWID	BASE32C-BASE95C	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	BASE32C-BASE95C	12.71	14.06	14.99	15.46	58.42	61.15
SO BUILDWID	BASE32C-BASE95C	28.64	30.02	30.48	0.00	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDHGT	LD5032C-LD7595C	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	LD5032C-LD7595C	0.00	0.00	0.00	6.71	6.71	14.33
SO BUILDHGT	LD5032C-LD7595C	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032C-LD7595C	14.33	14.33	14.33	14.33	15.24	15.24
SO BUILDHGT	LD5032C-LD7595C	15.24	15.24	15.24	0.00	0.00	0.00
SO BUILDHGT	LD5032C-LD7595C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032C-LD7595C	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	LD5032C-LD7595C	0.00	0.00	0.00	14.19	15.16	14.99
SO BUILDWID	LD5032C-LD7595C	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	LD5032C-LD7595C	12.71	14.06	14.99	15.46	58.42	61.15
SO BUILDWID	LD5032C-LD7595C	28.64	30.02	30.48	0.00	0.00	0.00
SO BUILDWID	LD5032C-LD7595C	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT	BASE32D-BASE95D	15.24	6.71	15.24	15.24	15.24	0.00
SO BUILDHGT	BASE32D-BASE95D	0.00	0.00	0.00	15.24	6.71	14.33
SO BUILDHGT	BASE32D-BASE95D	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32D-BASE95D	14.33	14.33	15.24	15.24	15.24	15.24
SO BUILDHGT	BASE32D-BASE95D	15.24	15.24	15.24	15.24	0.00	0.00
SO BUILDHGT	BASE32D-BASE95D	0.00	15.24	15.24	15.24	15.24	15.24
SO BUILDWID	BASE32D-BASE95D	30.02	12.97	47.77	53.91	58.42	0.00
SO BUILDWID	BASE32D-BASE95D	0.00	0.00	0.00	66.04	15.16	14.99
SO BUILDWID	BASE32D-BASE95D	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	BASE32D-BASE95D	12.71	14.06	29.48	30.40	30.40	29.48
SO BUILDWID	BASE32D-BASE95D	28.64	30.02	30.48	30.02	0.00	0.00
SO BUILDWID	BASE32D-BASE95D	0.00	64.02	67.49	28.64	30.02	30.48
SO BUILDHGT	LD5032D-LD7595D	15.24	6.71	15.24	15.24	15.24	0.00
SO BUILDHGT	LD5032D-LD7595D	0.00	0.00	0.00	15.24	6.71	14.33
SO BUILDHGT	LD5032D-LD7595D	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032D-LD7595D	14.33	14.33	15.24	15.24	15.24	15.24
SO BUILDHGT	LD5032D-LD7595D	15.24	15.24	15.24	15.24	0.00	0.00
SO BUILDHGT	LD5032D-LD7595D	0.00	15.24	15.24	15.24	15.24	15.24
SO BUILDWID	LD5032D-LD7595D	30.02	12.97	47.77	53.91	58.42	0.00
SO BUILDWID	LD5032D-LD7595D	0.00	0.00	0.00	66.04	15.16	14.99
SO BUILDWID	LD5032D-LD7595D	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	LD5032D-LD7595D	12.71	14.06	29.48	30.40	30.40	29.48
SO BUILDWID	LD5032D-LD7595D	28.64	30.02	30.48	30.02	0.00	0.00
SO BUILDWID	LD5032D-LD7595D	0.00	64.02	67.49	28.64	30.02	30.48

SO EMISUNIT .100000E+07 (GRAMS/SEC) (MICROGRAMS/CUBIC-METER)

SO SRCGROUP BASE32 BASE32A BASE32B BASE32C BASE32D

SO SRCGROUP BASE95 BASE95A BASE95B BASE95C BASE95D

SO SRCGROUP LD7532 LD7532A LD7532B LD7532C LD7532D

SO SRCGROUP LD7595 LD7595A LD7595B LD7595C LD7595D

SO SRCGROUP LD5032 LD5032A LD5032B LD5032C LD5032D

SO SRCGROUP LD5095 LD5095A LD5095B LD5095C LD5095D

SO FINISHED

RE STARTING

RE GRIDPOLR POL STA

RE GRIDPOLR POL ORIG 0.0 0.0

RE GRIDPOLR POL DIST 100 200 300 500 700 1000 1500 2000 2500 3000 4000 5000

RE GRIDPOLR POL DIST 7000 10000 12000 15000 20000 25000 30000

RE GRIDPOLR POL GDIR 36 10.00 10.00

RE GRIDPOLR POL END

RE FINISHED

ME STARTING

ME INPUTFIL D:\MET\TPAPRL87.BIN UNIFORM

ME ANEMHGT 6.700 METERS

ME SURFDATA 12842 1987 TAMPA

ME UAIRDATA 12842 1987 RUSKIN

ME WINDCATS 1.54 3.09 5.14 8.23 10.80

ME FINISHED

OU STARTING

OU RECTABLE ALLAVE FIRST

OU FINISHED

D:\PROJECTS\SONAT\LOAD\GENNGC1.187

8/25

CO STARTING

CO TITLEONE 1987 SONAT HARDEE COUNTY SITE, AT PSD CLASS 1 AREA 8/25/99

CO TITLETWO NATURAL GAS, GENERIC EMISSION RATES, 3 LOADS AND 2 TEMPERATURES

CO MODELOPT DFAULT CONC RURAL NOCMPL

CO AVERTIME PERIOD 24 8 3 1

CO POLLUTID GEN

CO DCAYCOEF .000000

CO RUNORNOT RUN

CO FINISHED

SO STARTING

** Source Location Cards:

** SRCID SRCTYP XS YS ZS

** MODELING ORIGIN CT 3 STACK LOCATION

** LOCATION IS USED FOR POLAR DISCRETE RECEPTORS.

** CT STACK NUMBER CODE

** -----

** B - CT 1

** C - CT 2

** D - CT 3

** E - CT 4

** Source Location Cards:

** SRCID SRCTYP XS YS ZS

** UTM (m) (m) (m)

SO LOCATION BASE32A POINT 408750. 3044500. 0.0

SO LOCATION BASE32B POINT 408750. 3044500. 0.0

SO LOCATION BASE32C POINT 408750. 3044500. 0.0

SO LOCATION BASE32D POINT 408750. 3044500. 0.0

SO LOCATION BASE95A POINT 408750. 3044500. 0.0

SO LOCATION BASE95B POINT 408750. 3044500. 0.0

SO LOCATION BASE95C POINT 408750. 3044500. 0.0

SO LOCATION BASE95D POINT 408750. 3044500. 0.0

SO LOCATION LD7532A POINT 408750. 3044500. 0.0

SO LOCATION LD7532B POINT 408750. 3044500. 0.0

SO LOCATION LD7532C POINT 408750. 3044500. 0.0

SO LOCATION LD7532D POINT 408750. 3044500. 0.0

SO LOCATION LD7595A POINT 408750. 3044500. 0.0

SO LOCATION LD7595B POINT 408750. 3044500. 0.0

SO LOCATION LD7595C POINT 408750. 3044500. 0.0

SO LOCATION LD7595D POINT 408750. 3044500. 0.0

SO LOCATION LD5032A POINT 408750. 3044500. 0.0

SO LOCATION LD5032B POINT 408750. 3044500. 0.0

SO LOCATION LD5032C POINT 408750. 3044500. 0.0

SO LOCATION LD5032D POINT 408750. 3044500. 0.0

SO LOCATION LD5095A POINT 408750. 3044500. 0.0

SO LOCATION LD5095B POINT 408750. 3044500. 0.0

SO LOCATION LD5095C POINT 408750. 3044500. 0.0

SO LOCATION LD5095D POINT 408750. 3044500. 0.0

** Source Parameter Cards:

** POINT: SRCID QS HS TS VS DS

** (g/s) (m) (K) (m/s) (m)

SO SRCPARAM BASE32A 2.5000 18.3 864.8 36.18 6.71

SO SRCPARAM BASE32B 2.5000 18.3 864.8 36.18 6.71

SO SRCPARAM BASE32C 2.5000 18.3 864.8 36.18 6.71

SO SRCPARAM BASE32D 2.5000 18.3 864.8 36.18 6.71

SO SRCPARAM BASE95A 2.5000 18.3 885.9 38.86 6.71

SO SRCPARAM BASE95B 2.5000 18.3 885.9 38.86 6.71

SO SRCPARAM BASE95C 2.5000 18.3 885.9 38.86 6.71

SO SRCPARAM BASE95D 2.5000 18.3 885.9 38.86 6.71

SO SRCPARAM LD7532A 2.5000 18.3 905.4 30.63 6.71

SO SRCPARAM LD7532B 2.5000 18.3 905.4 30.63 6.71

SO SRCPARAM LD7532C 2.5000 18.3 905.4 30.63 6.71

SO SRCPARAM LD7532D 2.5000 18.3 905.4 30.63 6.71

SO SRCPARAM LD7595A 2.5000 18.3 918.2 28.96 6.71

SO SRCPARAM LD7595B 2.5000 18.3 918.2 28.96 6.71

SO SRCPARAM LD7595C 2.5000 18.3 918.2 28.96 6.71

SO SRCPARAM LD7595D 2.5000 18.3 918.2 28.96 6.71

SO SRCPARAM LD5032A 2.5000 18.3 905.9 25.66 6.71

SO SRCPARAM LD5032B 2.5000 18.3 905.9 25.66 6.71

SO SRCPARAM LD5032C 2.5000 18.3 905.9 25.66 6.71

SO SRCPARAM LD5032D 2.5000 18.3 905.9 25.66 6.71

SO SRCPARAM LD5095A 2.5000 18.3 922.0 24.54 6.71

SO SRCPARAM LD5095B 2.5000 18.3 922.0 24.54 6.71

SO SRCPARAM LD5095C 2.5000 18.3 922.0 24.54 6.71

SO SRCPARAM LD5095D 2.5000 18.3 922.0 24.54 6.71

BEST AVAILABLE COPY

D:\PROJECTS\SONAT\LOAD\GENNGC1.187

8/25/

SO BUILDHGT	BASE32A-BASE95A	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	BASE32A-BASE95A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32A-BASE95A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32A-BASE95A	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32A-BASE95A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32A-BASE95A	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	BASE32A-BASE95A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32A-BASE95A	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDWID	BASE32A-BASE95A	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	BASE32A-BASE95A	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32A-BASE95A	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDHGT	LD5032A-LD7595A	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	LD5032A-LD7595A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032A-LD7595A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	LD5032A-LD7595A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032A-LD7595A	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032A-LD7595A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032A-LD7595A	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	LD5032A-LD7595A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032A-LD7595A	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDWID	LD5032A-LD7595A	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	LD5032A-LD7595A	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032A-LD7595A	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT	BASE32B-BASE95B	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	BASE32B-BASE95B	0.00	0.00	0.00	6.71	6.71	6.71
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32B-BASE95B	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32B-BASE95B	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32B-BASE95B	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	BASE32B-BASE95B	0.00	0.00	0.00	14.19	15.16	15.66
SO BUILDWID	BASE32B-BASE95B	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	BASE32B-BASE95B	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	BASE32B-BASE95B	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32B-BASE95B	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDHGT	LD5032B-LD7595B	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	LD5032B-LD7595B	0.00	0.00	0.00	6.71	6.71	6.71
SO BUILDHGT	LD5032B-LD7595B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032B-LD7595B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032B-LD7595B	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032B-LD7595B	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032B-LD7595B	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	LD5032B-LD7595B	0.00	0.00	0.00	14.19	15.16	15.66
SO BUILDWID	LD5032B-LD7595B	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	LD5032B-LD7595B	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	LD5032B-LD7595B	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032B-LD7595B	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT	BASE32C-BASE95C	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	0.00	0.00	6.71	6.71	14.33
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	15.24	15.24
SO BUILDHGT	BASE32C-BASE95C	15.24	15.24	15.24	0.00	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32C-BASE95C	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	0.00	0.00	14.19	15.16	14.99
SO BUILDWID	BASE32C-BASE95C	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	BASE32C-BASE95C	12.71	14.06	14.99	15.46	58.42	61.15
SO BUILDWID	BASE32C-BASE95C	28.64	30.02	30.48	0.00	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDHGT	LD5032C-LD7595C	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	LD5032C-LD7595C	0.00	0.00	0.00	6.71	6.71	14.33
SO BUILDHGT	LD5032C-LD7595C	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032C-LD7595C	14.33	14.33	14.33	14.33	15.24	15.24
SO BUILDHGT	LD5032C-LD7595C	15.24	15.24	15.24	0.00	0.00	0.00
SO BUILDHGT	LD5032C-LD7595C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032C-LD7595C	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	LD5032C-LD7595C	0.00	0.00	0.00	14.19	15.16	14.99
SO BUILDWID	LD5032C-LD7595C	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	LD5032C-LD7595C	12.71	14.06	14.99	15.46	58.42	61.15
SO BUILDWID	LD5032C-LD7595C	28.64	30.02	30.48	0.00	0.00	0.00
SO BUILDWID	LD5032C-LD7595C	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT	BASE32D-BASE95D	15.24	6.71	15.24	15.24	15.24	0.00
SO BUILDHGT	BASE32D-BASE95D	0.00	0.00	0.00	15.24	6.71	14.33
SO BUILDHGT	BASE32D-BASE95D	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32D-BASE95D	14.33	14.33	15.24	15.24	15.24	15.24
SO BUILDHGT	BASE32D-BASE95D	15.24	15.24	15.24	15.24	0.00	0.00
SO BUILDHGT	BASE32D-BASE95D	0.00	15.24	15.24	15.24	15.24	15.24
SO BUILDWID	BASE32D-BASE95D	30.02	12.97	47.77	53.91	58.42	0.00
SO BUILDWID	BASE32D-BASE95D	0.00	0.00	0.00	66.04	15.16	14.99
SO BUILDWID	BASE32D-BASE95D	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	BASE32D-BASE95D	12.71	14.06	29.48	30.40	30.40	29.48
SO BUILDWID	BASE32D-BASE95D	28.64	30.02	30.48	30.02	0.00	0.00
SO BUILDWID	BASE32D-BASE95D	0.00	64.02	67.49	28.64	30.02	30.48
SO BUILDHGT	LD5032D-LD7595D	15.24	6.71	15.24	15.24	15.24	0.00
SO BUILDHGT	LD5032D-LD7595D	0.00	0.00	0.00	15.24	6.71	14.33
SO BUILDHGT	LD5032D-LD7595D	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032D-LD7595D	14.33	14.33	15.24	15.24	15.24	15.24
SO BUILDHGT	LD5032D-LD7595D	15.24	15.24	15.24	15.24	0.00	0.00
SO BUILDHGT	LD5032D-LD7595D	0.00	15.24	15.24	15.24	15.24	15.24
SO BUILDWID	LD5032D-LD7595D	30.02	12.97	47.77	53.91	58.42	0.00
SO BUILDWID	LD5032D-LD7595D	0.00	0.00	0.00	66.04	15.16	14.99
SO BUILDWID	LD5032D-LD7595D	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	LD5032D-LD7595D	12.71	14.06	29.48	30.40	30.40	29.48
SO BUILDWID	LD5032D-LD7595D	28.64	30.02	30.48	30.02	0.00	0.00
SO BUILDWID	LD5032D-LD7595D	0.00	64.02	67.49	28.64	30.02	30.48

SO EMISUNIT .100000E+07 (GRAMS/SEC) (MICROGRAMS/CUBIC-METER)

SO SRCGROUP BASE32 BASE32A BASE32B BASE32C BASE32D

SO SRCGROUP BASE95 BASE95A BASE95B BASE95C BASE95D

SO SRCGROUP LD7532 LD7532A LD7532B LD7532C LD7532D

SO SRCGROUP LD7595 LD7595A LD7595B LD7595C LD7595D

SO SRCGROUP LD5032 LD5032A LD5032B LD5032C LD5032D

SO SRCGROUP LD5095 LD5095A LD5095B LD5095C LD5095D

SO FINISHED

RE STARTING

RE DISCCART 340300 3165700

RE DISCCART 340300 3167700

RE DISCCART 340300 3169800

RE DISCCART 340700 3171900

RE DISCCART 342000 3174000

RE DISCCART 343000 3176200

RE DISCCART 343700 3178300

RE DISCCART 342400 3180600

RE DISCCART 341100 3183400

RE DISCCART 339000 3183400

RE DISCCART 336500 3183400

RE DISCCART 334000 3183400

RE DISCCART 331500 3183400

RE FINISHED

ME STARTING

ME INPUTFIL D:\MET\TPAPRL87.BIN UNIFORM

ME ANEMHGT 6.700 METERS

ME SURFDATA 12842 1987 TAMPA

ME UAIRDATA 12842 1987 RUSKIN

ME WINDCATS 1.54 3.09 5.14 8.23 10.80

ME FINISHED

OU STARTING

OU RECTABLE ALLAVE FIRST

OU FINISHED

CO STARTING
 CO TITLEONE 1987 SONAT HARDEE COUNTY SITE, AT PSD CLASS I AREA 8/25/99
 CO TITLETWO FUEL OIL, GENERIC EMISSION RATES, 3 LOADS AND 2 TEMPERATURES
 CO MODELOPT DFAULT CONC RURAL NOCMPL
 CO AVERTIME PERIOD 24 8 3 1
 CO POLLUTID GEN
 CO DCAYCOEF .000000
 CO RUNORNOT RUN
 CO FINISHED

SO STARTING

** Source Location Cards:

** SRCID SRC TYP XS YS ZS
 ** MODELING ORIGIN CT 3 STACK LOCATION
 ** LOCATION IS USED FOR POLAR DISCRETE RECEPTORS.
 ** CT STACK NUMBER CODE

** B - CT 1
 ** C - CT 2
 ** D - CT 3
 ** E - CT 4

** Source Location Cards:

** SRCID	SRC TYP	XS (m)	YS (m)	ZS (m)
SO LOCATION	BASE32A POINT	408750.	3044500.	0.0
SO LOCATION	BASE32B POINT	408750.	3044500.	0.0
SO LOCATION	BASE32C POINT	408750.	3044500.	0.0
SO LOCATION	BASE32D POINT	408750.	3044500.	0.0
SO LOCATION	BASE95A POINT	408750.	3044500.	0.0
SO LOCATION	BASE95B POINT	408750.	3044500.	0.0
SO LOCATION	BASE95C POINT	408750.	3044500.	0.0
SO LOCATION	BASE95D POINT	408750.	3044500.	0.0
SO LOCATION	LD7532A POINT	408750.	3044500.	0.0
SO LOCATION	LD7532B POINT	408750.	3044500.	0.0
SO LOCATION	LD7532C POINT	408750.	3044500.	0.0
SO LOCATION	LD7532D POINT	408750.	3044500.	0.0
SO LOCATION	LD7595A POINT	408750.	3044500.	0.0
SO LOCATION	LD7595B POINT	408750.	3044500.	0.0
SO LOCATION	LD7595C POINT	408750.	3044500.	0.0
SO LOCATION	LD7595D POINT	408750.	3044500.	0.0
SO LOCATION	LD5032A POINT	408750.	3044500.	0.0
SO LOCATION	LD5032B POINT	408750.	3044500.	0.0
SO LOCATION	LD5032C POINT	408750.	3044500.	0.0
SO LOCATION	LD5032D POINT	408750.	3044500.	0.0
SO LOCATION	LD5095A POINT	408750.	3044500.	0.0
SO LOCATION	LD5095B POINT	408750.	3044500.	0.0
SO LOCATION	LD5095C POINT	408750.	3044500.	0.0
SO LOCATION	LD5095D POINT	408750.	3044500.	0.0

** Source Parameter Cards:

** POINT: SRCID	QS (g/s)	HS (m)	TS (K)	VS (m/s)	DS (m)	
SO SRCPARAM	BASE32A	2.500	18.3	853.2	37.31	6.71
SO SRCPARAM	BASE32B	2.500	18.3	853.2	37.31	6.71
SO SRCPARAM	BASE32C	2.500	18.3	853.2	37.31	6.71
SO SRCPARAM	BASE32D	2.500	18.3	853.2	37.31	6.71
SO SRCPARAM	BASE95A	2.500	18.3	878.2	35.05	6.71
SO SRCPARAM	BASE95B	2.500	18.3	878.2	35.05	6.71
SO SRCPARAM	BASE95C	2.500	18.3	878.2	35.05	6.71
SO SRCPARAM	BASE95D	2.500	18.3	878.2	35.05	6.71
SO SRCPARAM	LD7532A	2.500	18.3	905.4	30.78	6.71
SO SRCPARAM	LD7532B	2.500	18.3	905.4	30.78	6.71
SO SRCPARAM	LD7532C	2.500	18.3	905.4	30.78	6.71
SO SRCPARAM	LD7532D	2.500	18.3	905.4	30.78	6.71
SO SRCPARAM	LD7595A	2.500	18.3	914.3	29.57	6.71
SO SRCPARAM	LD7595B	2.500	18.3	914.3	29.57	6.71
SO SRCPARAM	LD7595C	2.500	18.3	914.3	29.57	6.71
SO SRCPARAM	LD7595D	2.500	18.3	914.3	29.57	6.71
SO SRCPARAM	LD5032A	2.500	18.3	922.0	26.12	6.71
SO SRCPARAM	LD5032B	2.500	18.3	922.0	26.12	6.71
SO SRCPARAM	LD5032C	2.500	18.3	922.0	26.12	6.71
SO SRCPARAM	LD5032D	2.500	18.3	922.0	26.12	6.71
SO SRCPARAM	LD5095A	2.500	18.3	922.0	24.84	6.71
SO SRCPARAM	LD5095B	2.500	18.3	922.0	24.84	6.71
SO SRCPARAM	LD5095C	2.500	18.3	922.0	24.84	6.71
SO SRCPARAM	LD5095D	2.500	18.3	922.0	24.84	6.71

SO BUILDHGT	BASE32A-BASE95A	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	BASE32A-BASE95A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32A-BASE95A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	BASE32A-BASE95A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32A-BASE95A	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32A-BASE95A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32A-BASE95A	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	BASE32A-BASE95A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32A-BASE95A	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDWID	BASE32A-BASE95A	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	BASE32A-BASE95A	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32A-BASE95A	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDHGT	LD5032A-LD7595A	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	LD5032A-LD7595A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032A-LD7595A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDHGT	LD5032A-LD7595A	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032A-LD7595A	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032A-LD7595A	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032A-LD7595A	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	LD5032A-LD7595A	0.00	0.00	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032A-LD7595A	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDWID	LD5032A-LD7595A	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	LD5032A-LD7595A	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032A-LD7595A	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT	BASE32B-BASE95B	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	BASE32B-BASE95B	0.00	0.00	0.00	6.71	6.71	6.71
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32B-BASE95B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	BASE32B-BASE95B	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	BASE32B-BASE95B	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32B-BASE95B	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	BASE32B-BASE95B	0.00	0.00	0.00	14.19	15.16	15.66
SO BUILDWID	BASE32B-BASE95B	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	BASE32B-BASE95B	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	BASE32B-BASE95B	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	BASE32B-BASE95B	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDHGT	LD5032B-LD7595B	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	LD5032B-LD7595B	0.00	0.00	0.00	6.71	6.71	6.71
SO BUILDHGT	LD5032B-LD7595B	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032B-LD7595B	14.33	14.33	14.33	14.33	14.33	14.33
SO BUILDHGT	LD5032B-LD7595B	6.71	6.71	0.00	0.00	0.00	0.00
SO BUILDHGT	LD5032B-LD7595B	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032B-LD7595B	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	LD5032B-LD7595B	0.00	0.00	0.00	14.19	15.16	15.66
SO BUILDWID	LD5032B-LD7595B	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	LD5032B-LD7595B	12.71	14.06	14.99	15.46	15.46	14.99
SO BUILDWID	LD5032B-LD7595B	15.16	14.19	0.00	0.00	0.00	0.00
SO BUILDWID	LD5032B-LD7595B	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT	BASE32C-BASE95C	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	0.00	0.00	6.71	6.71	14.33
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32C-BASE95C	14.33	14.33	14.33	14.33	15.24	15.24
SO BUILDHGT	BASE32C-BASE95C	15.24	15.24	15.24	0.00	0.00	0.00
SO BUILDHGT	BASE32C-BASE95C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	BASE32C-BASE95C	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	0.00	0.00	14.19	15.16	14.99
SO BUILDWID	BASE32C-BASE95C	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	BASE32C-BASE95C	12.71	14.06	14.99	15.46	58.42	61.15
SO BUILDWID	BASE32C-BASE95C	28.64	30.02	30.48	0.00	0.00	0.00
SO BUILDWID	BASE32C-BASE95C	0.00	15.23	14.32	12.97	11.23	9.14
SO BUILDHGT	LD5032C-LD7595C	6.71	6.71	6.71	14.33	0.00	0.00
SO BUILDHGT	LD5032C-LD7595C	0.00	0.00	0.00	6.71	6.71	14.33
SO BUILDHGT	LD5032C-LD7595C	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032C-LD7595C	14.33	14.33	14.33	14.33	15.24	15.24
SO BUILDHGT	LD5032C-LD7595C	15.24	15.24	15.24	0.00	0.00	0.00
SO BUILDHGT	LD5032C-LD7595C	0.00	6.71	6.71	6.71	6.71	6.71
SO BUILDWID	LD5032C-LD7595C	11.23	12.97	14.32	15.46	0.00	0.00
SO BUILDWID	LD5032C-LD7595C	0.00	0.00	0.00	14.19	15.16	14.99
SO BUILDWID	LD5032C-LD7595C	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	LD5032C-LD7595C	12.71	14.06	14.99	15.46	58.42	61.15
SO BUILDWID	LD5032C-LD7595C	28.64	30.02	30.48	0.00	0.00	0.00
SO BUILDWID	LD5032C-LD7595C	0.00	15.23	14.32	12.97	11.23	9.14

SO BUILDHGT	BASE32D-BASE95D	15.24	6.71	15.24	15.24	15.24	0.00
SO BUILDHGT	BASE32D-BASE95D	0.00	0.00	0.00	15.24	6.71	14.33
SO BUILDHGT	BASE32D-BASE95D	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	BASE32D-BASE95D	14.33	14.33	15.24	15.24	15.24	15.24
SO BUILDHGT	BASE32D-BASE95D	15.24	15.24	15.24	15.24	0.00	0.00
SO BUILDHGT	BASE32D-BASE95D	0.00	15.24	15.24	15.24	15.24	15.24
SO BUILDWID	BASE32D-BASE95D	30.02	12.97	47.77	53.91	58.42	0.00
SO BUILDWID	BASE32D-BASE95D	0.00	0.00	0.00	66.04	15.16	14.99
SO BUILDWID	BASE32D-BASE95D	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	BASE32D-BASE95D	12.71	14.06	29.48	30.40	30.40	29.48
SO BUILDWID	BASE32D-BASE95D	28.64	30.02	30.48	30.02	0.00	0.00
SO BUILDWID	BASE32D-BASE95D	0.00	64.02	67.49	28.64	30.02	30.48
SO BUILDHGT	LD5032D-LD7595D	15.24	6.71	15.24	15.24	15.24	0.00
SO BUILDHGT	LD5032D-LD7595D	0.00	0.00	0.00	15.24	6.71	14.33
SO BUILDHGT	LD5032D-LD7595D	14.33	14.33	14.33	14.33	6.71	6.71
SO BUILDHGT	LD5032D-LD7595D	14.33	14.33	15.24	15.24	15.24	15.24
SO BUILDHGT	LD5032D-LD7595D	15.24	15.24	15.24	15.24	0.00	0.00
SO BUILDHGT	LD5032D-LD7595D	0.00	15.24	15.24	15.24	15.24	15.24
SO BUILDWID	LD5032D-LD7595D	30.02	12.97	47.77	53.91	58.42	0.00
SO BUILDWID	LD5032D-LD7595D	0.00	0.00	0.00	66.04	15.16	14.99
SO BUILDWID	LD5032D-LD7595D	15.46	15.46	14.99	14.06	11.23	9.14
SO BUILDWID	LD5032D-LD7595D	12.71	14.06	29.48	30.40	30.40	29.48
SO BUILDWID	LD5032D-LD7595D	28.64	30.02	30.48	30.02	0.00	0.00
SO BUILDWID	LD5032D-LD7595D	0.00	64.02	67.49	28.64	30.02	30.48

SO EMISUNIT .100000E+07 (GRAMS/SEC) (MICROGRAMS/CUBIC-METER)

SO SRCGROUP BASE32 BASE32A BASE32B BASE32C BASE32D

SO SRCGROUP BASE95 BASE95A BASE95B BASE95C BASE95D

SO SRCGROUP LD7532 LD7532A LD7532B LD7532C LD7532D

SO SRCGROUP LD7595 LD7595A LD7595B LD7595C LD7595D

SO SRCGROUP LD5032 LD5032A LD5032B LD5032C LD5032D

SO SRCGROUP LD5095 LD5095A LD5095B LD5095C LD5095D

SO FINISHED

RE STARTING

RE DISCCART 340300 3165700

RE DISCCART 340300 3167700

RE DISCCART 340300 3169800

RE DISCCART 340700 3171900

RE DISCCART 342000 3174000

RE DISCCART 343000 3176200

RE DISCCART 343700 3178300

RE DISCCART 342400 3180600

RE DISCCART 341100 3183400

RE DISCCART 339000 3183400

RE DISCCART 336500 3183400

RE DISCCART 334000 3183400

RE DISCCART 331500 3183400

RE FINISHED

ME STARTING

ME INPUTFIL D:\MET\TPAPRL87.BIN UNIFORM

ME ANEMHGT 6.700 METERS

ME SURFDATA 12842 1987 TAMPA

ME UAIRDATA 12842 1987 RUSKIN

ME WINDCATS 1.54 3.09 5.14 8.23 10.80

ME FINISHED

OU STARTING

OU RECTABLE ALLAVE FIRST SECOND

OU FINISHED