

POB 2436
 LC 32055-

Public Notice

JA 1304,
 a 21st day

Three hours	416	81 percent
24 hours	79	87 percent
Annual	8	40 percent

A person who is substantially affected by the Department's proposed permitting decision may request a hearing in accordance with Section 120.57, Florida Statutes, and Chapter 17-1 and 28-5 Florida Administrative Code. The request for hearing must be filed (received) in the Office of General Counsel of the Department at 2600 Blair Stone Road, Twin Towers Office Building, Tallahassee, FL 32301, within (14) days of publication of this notice. Failure to file a request for hearing within this time period shall constitute a waiver of any right such person may have to request hearing under Section 120.57, Florida Statutes.

By authority of the U.S. Environmental Protection Agency, the Florida Department of Environmental Regulation (FDER) has reviewed the proposed construction under Federal Prevention of Significant Deterioration Regulations (40 CFR 52.21). The FDER has made a preliminary determination that the construction can be approved provided certain conditions are met. A summary of the basis for this determination and the application for a permit submitted by Occidental Chemical Company are available for public review in the following FDER offices:

Department of Environmental Regulation
 Northeast District
 3426 Hills Road
 Jacksonville, FL 32207

Department of Environmental Regulation
 2600 Blair Stone Road
 Tallahassee, FL 32301

Columbia County Public Library
 490 N. Columbia Street
 Lake City, FL 32052

Any person may send written comments on the proposed action to Mr. Clair Fancy at the Department's Tallahassee address. All comments mailed within 30 days of publication of this notice will be considered in the Department's final determination.

No. 3355
 March 31, 1983

... II
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 ... te Attorney

... 31, 1983
 ... 7, 1983

NOTICE OF PROPOSED AGENCY ACTION

3/31/83
Lake City, Florida

The Department of Environmental Regulation gives notice of its intent to issue permits to Occidental Chemical Company. These permits will allow an increase in the production rate of two existing sulfuric acid plants and the use of fuel oil containing a higher percentage of sulfur than they are currently permitted to use in four existing steam boilers and a diammonium phosphate dryer. These sources are located at the Suwannee River (SRCC) and Swift Creek Chemical Complexes (SCCC) near White Springs in Hamilton County, Florida. No physical modifications to the plant equipment are required to accomplish these operational changes except for the minor changes detailed in the construction permit application.

A best available control technology (BACT) determination was required for sulfur dioxide (SO2).

Emission of criteria pollutants from the two chemical complexes will increase by the quantities in tons per year (TPY),

SO2	802
SRCC	443.9
SCCC	951

Emissions from the modified sources will consume increment but will not violate any state or federal ambient air quality standards. The maximum increment consumption in micrograms per cubic meter (ug/m3), and percent of available increment are listed below.

SO2	SRCC	
	ug/m3	
Three hours	258	50 percent
24 hours	73	80 percent
Annual	12	60 percent
	SCCC	
	ug/m3	

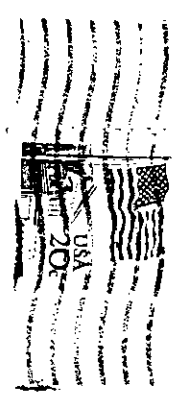
MR. John Sweeney

FDER - Air Quality

Twin Towers Bldg

2600 Blair Stone Rd

Tallahassee 32301



4/23/83

APR 27 1983

DEAR John

EAON

Thank you for sending
the OCC permit request
information — hopefully
we'll have some comments
to contribute —

Am also sending along
a picture of a Swanee
tributary creek in Columbia
County, a Super nice
stream — the headwaters
of this creek are in the
Osceola Forest & in one
of the "proposed" lease
areas, naturally — it's
nice in the Forest, too!

Will be back in touch —

Regards —

Judy Hancock



** ORIGINAL PHOTOS ARE IN "SUPPLEMENTAL DOCUMENTS"
DRAWER: OCCIDENTAL CHEMICAL CORPORATION
AC 24-56209, -10, -11, -12, -13, -14, -15
PSDFL-082, -083

①

Robinson Branch -
Osceola Forest -

This is also a
tributary creek to
the Swannoe &
has a nice water fall
at the river below
Big Shoals - This
creek is on Kerr -
McGees claimed "lease"
area ^{in the forest} & they own it
at the confluence with
the Swannoe
4/19/83

②

Falling Creek -
Tributary to the
Swannoe in
Columbia County

4/18/83

"
** ORIGINAL PHOTOS ARE IN SUPPLEMENTAL DOCUMENTS "

DRAWER : OCCIDENTAL CHEMICAL ~~TRADING~~ CORPORATION

AC 24 - 56209, 10, 11, 12, - B, 14, - 15

PSDFL - 082, - 083

THE LAKE CITY REPORTER

Lake City, Columbia County, Florida

STATE OF FLORIDA,
COUNTY OF COLUMBIA.

Before the undersigned authority personally appeared Don L. Caldwell

who on oath says that he is Publisher of the Lake City Reporter, a newspaper published at Lake City, Columbia County, Florida; that the attached copy of advertisement, being a legal advertisement

in the matter of Notice of Proposed Agency Action

in the _____ Court, was published in said newspaper in the issues of _____

March 31, 1983

Affiant further says that The Lake City Reporter is a newspaper published at Lake City in said Columbia County, Florida, and that the said newspaper has heretofore been continuously published in said Columbia County, Florida, and has been entered as second class mail matter at the post office in Lake City, in said Columbia County, Florida, for a period of one year next preceding the first publication of the attached copy of advertisement; and affiant further says that he has neither paid nor promised any person, firm or corporation any discount, rebate, commission or refund for the purpose of securing this advertisement for publication in the said newspaper.

Sworn to and subscribed before me this 31 day of March

A. D., 19 83

Don L. Caldwell

Vicki H. Her

Notary Public

Notary Public, State of Florida at Large
My Commission Expires September 15, 1985

Pat Summerall Printing - No. 8559

D 57
APR 04 1983
BAQM

NOTICE OF PROPOSED AGENCY ACTION

The Department of Environmental Regulation gives notice of its intent to issue permits to Occidental Chemical Company. These permits will allow an increase in the production rate of two existing sulfuric acid plants and the use of fuel oil containing a higher percentage of sulfur than they are currently permitted to use in four existing steam boilers and a ammonium phosphate dryer. These sources are located at the Suwannee River (SRCC) and Swift Creek Chemical Complex (SCCC) near White Springs in Hamilton County, Florida. No physical modifications to the plant equipment are required to accomplish these operational changes except for the minor changes detailed in the construction permit application.

A best available control technology (BACT) determination was required for sulfur dioxide (SO2).

Emission of criteria pollutants from the two chemical complexes will increase by the quantities in tons per year (TPY).

SRCC	802
SCCC	443.9
SCCC	961

Emissions from the modified sources will consume increment but will not violate any state or federal ambient air quality standards. The maximum increment consumption in micrograms per cubic meter (ug/m3), and percent of available increment are listed below.

	ug/m3	
SRCC		
Three hours	256	50 percent
24 hours	79	80 percent
Annual	13	88 percent

SCCC		
Three hours	256	50 percent
24 hours	79	80 percent
Annual	13	88 percent

Three hours	416	81 percent
24 hours	79	87 percent
Annual	8	46 percent

A person who is substantially affected by the Department's proposed permitting decision may request a hearing in accordance with Section 120.57, Florida Statutes, and Chapter 17-1 and 28-6 Florida Administrative Code. The request for hearing must be filed (received) in the Office of General Counsel of the Department at 2800 Blair Stone Road, Twin Towers Office Building, Tallahassee, FL 32301, within (14) days of publication of this notice. Failure to file a request for hearing within this time period shall constitute a waiver of any right such person may have to request hearing under Section 120.57, Florida Statutes.

By authority of the U.S. Environmental Protection Agency, the Florida Department of Environmental Regulation (FDER) has reviewed the proposed construction under Federal Prevention of Significant Deterioration Regulations (40 CFR 52.21). The FDER has made a preliminary determination that the construction can be approved provided certain conditions are met. A summary of the basis for this determination and the application for a permit submitted by Occidental Chemical Company are available for public review in the following FDER offices:

Department of Environmental Regulation
Northeast District
3428 Bills Road
Jacksonville, FL 32207

Department of Environmental Regulation
2800 Blair Stone Road
Tallahassee, FL 32301

Columbia County Public Library
600 N. Columbia Street
Lake City, FL 32062

Any person may send written comments on the proposed action to Mr. Clair Fancy of the Department's Tallahassee address. All comments mailed within 30 days of publication of this notice will be considered in the Department's final determination.

No. 3255
March 31, 1983



SHOLTÈS & KOOGLER, ENVIRONMENTAL CONSULTANTS
1213 N.W. 6th Street Gainesville, Florida 32601 (904) 377-5822

SKEC 102-81-08

December 16, 1982

*Bill
Teresa*

Mr. Clair Fancy
Florida Department of
Environmental Regulation
Twin Towers Office Building
2600 Blair Stone Road
Tallahassee, FL 32301

Subject: Occidental Chemical Company
Hamilton County, Florida
Preliminary Determination PSD-FL-082
Preliminary Determination PSD-FL-083

Dear Mr. Fancy:

On November 18, 1982, Mr. Wes Atwood and I visited your office to discuss the two subject PSD Applications and the FDER Air Pollution Source Construction Permits associated with the sources addressed in these applications. I would like to provide you with a written record of the matters which we discussed and provide you with documentation to support our comments.

PSD-FL-082

A request was made to modify the Public Notice contained in this application. The last sentence in the first paragraph of the Notice read, "No physical modifications to the plant equipment is required to accomplish these operational changes." We requested that this sentence be reworded to read, "No physical modifications to the plant equipment are required to accomplish these operational changes except for the minor changes detailed in the construction permit applications." The construction permit applications referenced are those for sulfuric acid plant "E" (AC24-56211) and sulfuric acid plant "F" (AC24-56209). The modifications are described on Page 2A of these applications and relate to modifications to handle the increased gas flow rate through the sulfuric acid plants.

Specific condition No. 5 of both sulfuric acid plant construction permits (referenced in the above paragraph) require that the applicant establish a conversion factor that requires a measurement of the sulfur dioxide concentration at the converter entrance. This conversion factor is then used with the continuous stack gas sulfur dioxide monitoring data to calculate a sulfur dioxide emission rate with units of pounds of sulfur dioxide per ton of acid produced.

Occidental has worked with EPA for quite some time to have an alternative method approved for calculating the sulfur dioxide emission rate per ton of acid produced. This method was proposed as an alternative to 40 CFR 60.84 in the Federal Register of July 16, 1982; a copy of which is attached. This method requires only that the sulfur dioxide and the oxygen concentrations be measured in the stack gas. These concentrations can then be used with the equation published in the Federal Register to calculate the pounds of sulfur dioxide emitted per ton of acid produced. To facilitate the use of the method published in the Federal Register, Occidental has installed continuous oxygen monitors on both the "E" and "F" sulfuric acid plant stacks. In the case of Occidental there is no auxiliary fuel used in the sulfuric acid plants, hence the "auxiliary fuel factor" used in the equation published in the Federal Register is equal to 0.00.

Occidental is of the opinion that the method published in the Federal Register is much easier to use than the method presently specified in the draft construction permits and requests that the method published in the Federal Register be substituted for the method presently proposed in specific condition No. 5. If you have any questions regarding the derivation of the method published in the Federal Register or any other questions regarding this method, please feel free to contact me.

Specific condition No. 9 of the draft construction permits for both sulfuric acid plants requires that compliance for emission limits be determined in accordance with specific test methods. For nitrogen oxide EPA Test Method 7 is specified. Nowhere in specific condition No. 9 or any other specific conditions attached to the permits does it specify the frequency with which compliance tests must be made.

It is requested that a condition to demonstrate compliance with the emission limit for nitrogen oxides be worded similar to the specific condition attached to the construction permit for auxiliary boiler "E"; also covered by PSD Application PSD-FL-082. This condition is worded, "Performance tests for nitrogen oxides. . . to determine emission compliance status shall be requested by the Department when deemed necessary."

PSD-FL-083

A typographical error was noted in Table 1 of the Preliminary Determination for this application. The "worst case" particulate matter emission rate for the "C" boiler, as proposed, will be 46.7 tons per year. This will result in an increase of 7.2 tons per year over the currently permitted emission rate. This increase, combined with other increases addressed in the PSD Application, will result in a total particulate matter increase for all sources addressed by the Application of 6.7 tons per year.

Specific condition No. 2 of the construction permit applications for boiler "C" (AC24-56214) and boiler "D" (AC24-56213) specify that the boilers shall be allowed to operate 25 percent of the time. Occidental requests that the 0.25 annual operating factor be removed as a permit condition. The entire Air Quality Review which is part of the subject PSD Application, was conducted under the assumption that both boilers would operate 100 percent of the time. The conclusion reached in the Application was that all of the modifications addressed could be approved with no threat to ambient air quality standards or to PSD increments.

The "25 percent" condition first appeared in an operating permit for either the "C" or "D" boiler and was stated ". . . the boiler will operate about 25 percent of the time." This condition came about, to the best of our knowledge as a result of a response to an inquiry by the Jacksonville FDER office regarding the approximate operating time of the boilers. At no time were the operating times of these boilers limited because of a threat to ambient air quality.

The original approval to construct the boilers, granted by EPA on March 21, 1978, did not limit the operating time of the "C" and "D" boilers, nor did the original state construction permits (AC24-2700 and 2701). The original operating permits for the boilers also did not limit the time of operation of the boilers and a construction permit granted to allow the use of a coal-oil mix in the "C" boiler (AC24-40968) issued on June 30, 1981, did not limit the operating time of this boiler.

In view of this history and the fact that we can uncover no concrete reason for the 0.25 annual operating factor to be a part of the construction permits for either the "C" or "D" boilers, Occidental requests that these conditions be removed.

Mr. Clair Fancy
Florida Department of Environmental Regulation

December 16, 1982
Page four

If there are any questions regarding the matter addressed in this letter, please feel free to contact me.

Very truly yours,

SHOLTES & KOGLER
ENVIRONMENTAL CONSULTANTS, INC.



John B. Koogler, Ph.D., P.E.

JBK:sc
Attachments

cc: Mr. W. W. Atwood

40 CFR Part 60

[AD-FRL-2145-3]

Standards of Performance for New Stationary Sources; Alternative Sampling Procedures for Sulfuric Acid Plants

AGENCY: Environmental Protection Agency (EPA).

ACTION: Proposed rule.

SUMMARY: The purpose of this action is to propose an alternative procedure for determining the SO₂ or sulfuric acid mist emission rate based on measurements of O₂ and SO₂ or acid mist concentrations in the plant exhaust.

These revisions would apply to all sources subject to the standards of performance for sulfuric acid plants.

DATE: *Comments.* Comments must be received on or before September 14, 1982.

Public Hearing. A public hearing will be held, if requested. Persons wishing to request a public hearing must contact EPA by August 16, 1982. If a hearing is requested, an announcement of the date and place will appear in a separate Federal Register notice.

ADDRESS: *Comments.* Comments should be submitted (in duplicate if possible) to: Central Docket Section (A-133), Attention: Docket Number A-82-03, U.S. Environmental Protection Agency, 401 M Street, SW., Washington, D.C. 20460.

Public Hearing. Persons wishing to present oral testimony should notify Mrs. Naomi Durkee, Emission Standards and Engineering Division (MD-13), U.S. Environmental Protection Agency, Research Triangle Park, North Carolina 27711, telephone number (919) 541-5578.

Docket. Docket No. A-82-03, containing materials relevant to this rulemaking, is available for public inspection and copying between 8:00 a.m. and 4:00 p.m., Monday through Friday, at EPA's Central Docket Section, West Tower Lobby, Gallery 1, Waterside Mall, 401 M Street, SW.,

Washington, D.C. 20460. A reasonable fee may be charged for copying.

FOR FURTHER INFORMATION CONTACT: Mr. Roger Shigehara, Emission Measurement Branch (MD-13), Emission Standards and Engineering Division, U.S. Environmental Protection Agency, Research Triangle Park, North Carolina 27711, telephone number (919) 541-2300.

SUPPLEMENTARY INFORMATION: Subpart H of 40 CFR Part 60 contains standards of performance for the sulfuric acid manufacturing plant industry including sulfur dioxide (SO₂) and sulfuric acid mist emission rate limits and continuous monitoring requirements. Data from emission measurement tests and continuous monitoring systems must be converted from units of SO₂ or sulfuric acid mist concentrations to the units of the standard in kg per metric ton of acid produced (lb per short ton). The present procedure for this conversion requires the measurement of the inlet SO₂ to the plant converter and the calculation of a production rate factor in kg per metric ton per ppm (lb per short ton per ppm) for each 8-hour period.

The proposed revisions allow the source to measure O₂ concentration in the exhaust gas as an alternative to measurements of SO₂ inlet concentrations and process production rates in obtaining SO₂ or sulfuric acid mist emission rates from sulfuric acid plants. The procedure is applicable to plants that oxidize elemental sulfur or oxidize ore that contains elemental sulfur. The procedure does not apply to plants which use spent acid or use gas streams containing hydrogen sulfide in the production of acid.

The alternative procedure is based on a sulfur mass balance determination of the sulfuric acid production process. It is accurate to the accuracy level of the measurements. The revision is appropriate for the applicable plants, and it provides a means of reducing the testing requirements without loss of emissions data.

These revisions would apply to all sources subject to the standards of performance for sulfuric acid plants. This rulemaking would not impose any additional emission measurement requirements on any facilities. Rather, the rulemaking would simply revise the emission measurement calculation procedures allowing an alternative to procedures that would apply irrespective of this rulemaking.

The Office of Management and Budget has exempted this rule from the requirements of Section 3 of Executive Order 12291.

Pursuant to the provisions of 5 U.S.C. 605(b), I hereby certify that this rule will not have a significant economic impact on a substantial number of small entities.

(Sec. 111, 114, and 301(a) of the Clean Air Act, as amended (42 U.S.C. 7411, 7414, and 7601(a))

Dated: July 7, 1982.

Anne M. Gorsuch,
Administrator.

Lists of Subjects in 40 CFR Part 60

Air pollution control, Aluminum, Ammonium sulfate plants, Cement industry, Coal, Copper, Electric power plants, Glass and glass products, Grains, Intergovernmental relations, Iron, Lead, Metals, Motor vehicles, Nitric acid plants, Paper and paper products industry, Petroleum, Phosphate, Sewage disposal, Steel, Sulfuric acid plants, Waste treatment and disposal, Zinc.

PART 60—STANDARDS OF PERFORMANCE FOR NEW STATIONARY SOURCES

It is proposed that Subpart H of 40 CFR Part 60 be amended as follows:

1. By adding a paragraph (d) to § 60.84 as follows:

§ 60.84 Emission monitoring.

(d) Alternatively, a source that processes elemental sulfur or an ore that contains elemental sulfur may use the following continuous emission monitoring approach and calculation procedures in determining SO₂ emissions rates in terms of the standard. Continuous emission monitoring of SO₂, O₂, and CO₂ (if required) shall be installed, calibrated, maintained, and operated by the owner or operator according to this procedure in Performance Specifications 2 and 3. This calibration procedure and span value for this SO₂ monitor shall be as specified in paragraph (b) of this section. This span value for CO₂ (if required) shall be 10 percent and for O₂ shall be 20.9 percent (air). A conversion factor based on process rate data is not necessary. Calculate the SO₂ emission rate as follows:

$$E_{SO_2} = C_{SO_2} \times S \times \frac{1}{0.263 - 0.0126(O_2) - A(CO_2)}$$

Where:

E_{SO₂} = SO₂ emission rate, kg/t acid (lb/ton acid).

C_{SO₂} = SO₂ concentration, kg/dscm (lb/dscf) (see Table below).

S = Acid production rate factor.
= 355 dscm/t acid for metric units.
= 11600 dscf/ton acid for English units.

of Oxygen

O₂ = O₂ concentration, percent.

- A = Auxiliary fuel factor.
- = 0.00 for no fuel.
- = 0.0226 for methane.
- = 0.0217 for natural gas.
- = 0.0196 for propane.
- = 0.0172 for #2 oil.
- = 0.0161 for #6 oil.
- = 0.0148 for coal.
- = 0.0126 for coke.

CO₂ = CO₂ concentration, percent.

Note.—It is necessary in some cases to convert measured concentration units to other units for these calculations:

Use the following Table for such conversions:

From—	To—	Multiply by—
g/dscm	kg/dscm	10 ⁻³
mg/dscm	kg/dscm	10 ⁻⁶
ppm(SO ₂)	kg/dscm	2.660 × 10 ⁻⁶
ppm(SO ₂)	lb/dscf	1.650 × 10 ⁻⁷

2. By adding a paragraph (e) to § 60.85 as follows:

§ 60.85 Test methods and procedures.

(e) Alternatively, a source that processes elemental sulfur or an ore that contains elemental sulfur may use the SO₂, acid mist, O₂, and CO₂ (if required) measurement data in determining SO₂ and acid mist emission rates in terms of the standard. Data from the reference method tests as specified in (a) of this part are required; that is, Method 8 for SO₂ and acid mist and Method 3 for O₂ and CO₂. No determinations of production rate or total gas flow rate are necessary. Calculate the SO₂ and acid mist emission rate as described in § 60.84(d) substituting the acid mist concentration for C_{SO₂} as appropriate.

[FR Doc. 82-19406 Filed 7-15-82; 9:45 am]

BILLING CODE 6560-50-M

Best Available Control Technology (BACT) Determination
Part I of III
Occidental Chemical Company
Hamilton County

The applicant plans to increase production from the sulfuric acid plants "E" and "F" located at their fertilizer grade phosphate rock processing facility at the Swift Creek Chemical Complex near White Springs, Florida. The production capacity of each acid plant is to be increased 25 percent to 2500 tons per day of 100% acid. Both acid plants have inherent in the initial design a production rate of 2300 tons per day with no major equipment modifications. It will be necessary to modify the economizer, gas handling and catalyst loading systems to achieve the 2500 tons per day production rate.

Air pollutants emitted from the sulfuric acid plants will be SO₂, NO_x, CO and sulfuric acid mist increasing the annual ambient air burden by 730,26,1, and 27 tons, respectively. Sulfur dioxide and sulfuric acid mist emissions increase exceeds the significant emission rate and requires a Best Available Control Technology determination as set forth in 17-2.500(2)(f), FAC.

The applicant has submitted several applications that require a BACT determination. Three determinations have been made by combining similar sources as follows:

- PART I - Sulfuric Acid Plants,
- PART II - Boiler Fuel Conversions
- PART III - DAP Dryer Fuel Conversion.

BACT Determination Requested by the Applicant:

Sulfuric Acid Plant E and F.

<u>Pollutant</u>	<u>Emission Limit</u>
SO ₂	4.0 lb/ton 100% acid
H ₂ SO ₄ mist	0.15 lb/ton 100% acid

Sulfur dioxide emissions will be controlled by double absorption with catalyst screening and make up every three to five years.

Sulfuric acid mist emissions will be controlled with HV mist eliminators.

Date of Receipt of a BACT application:

May 27, 1982

Date of Publication in the Florida Administrative Weekly:

June 11, 1982

Review Group Members:

The final determination was based upon comments received from the New Source Review Section and the Air Modeling Section.

BACT Determined by DER:

Sulfur dioxide emissions from sulfuric acid plants E and F not to exceed 4 pounds per tons of 100% sulfuric acid produced.

Sulfuric acid mist emissions from sulfuric acid plants E and F not to exceed 0.15 pounds per ton of 100% sulfuric acid produced.

Visible emissions to be less than 10% opacity.

Test methods and procedures per the NSPS, 40 CFR Part 60, Subpart H, Subsections 60.84 and 60.85.

Justification of DER Determination:

Sulfur dioxide and sulfuric acid mist emissions are subject to standards of performance for sulfuric acid plants (40 CFR 60.80) promulgated in 1971. U. S. EPA reviewed the standard in 1979 (44 FR15742) and decided not to change the emission limits.

BACT for the sulfuric acid plants E and F is determined to be equal to New Source Performance Standards (NSPS) for sulfuric acid plants, 40 CFR 60, Subpart H.

Details of the Analysis May Be Obtained by Contacting:

Edward Palagyi, BACT Coordinator
Department of Environmental Regulation
Bureau of Air Quality Management
2600 Blair Stone Road
Tallahassee, Florida 32301

Recommended By:

for (H) Joney

Steve Smallwood, Chief BAQM

Date: 11/7/82

Approved:

Victoria J. Tschinkel

Victoria J. Tschinkel, Secretary

Date: 11/18/82

Best Available Control Technology (BACT) Determination
Part II of III
Occidental Chemical Company
Hamilton County

The applicant plans to fire a higher sulfur content fuel in four fossil-fuel fired steam generators located at their facilities near White Springs, Florida. Boiler E is at the Swift Creek Complex and boilers B, C, D are at the Suwannee River Complex. The existing sources are as follows.

1. Gas fired auxiliary steam boiler "B" is rated at 160 million BTU per hour heat input. The steam produced is used to augment the steam produced by the sulfuric acid plants B and C. Boiler B is operated at 25% of rated capacity when the sulfuric acid plants are in operation. No. 6 oil is used as a stand-by fuel, the sulfur content of which is limited by permit conditions at 0.8% maximum.

2. Gas fired auxiliary steam boiler "C" is rated at 120 million BTU per hour heat input. The steam produced is used in the superphosphoric acid evaporators. No. 6 oil is used as a stand-by fuel, the sulfur content of which is limited by permit conditions at 0.8% maximum.

Boiler "C" has recently been modified to fire a coal-oil mixture (COM), also a stand-by fuel for this unit. The sulfur content of the COM is limited by permit conditions at 0.7% maximum.

3. Gas fired auxiliary steam boiler "D" is rated at 120 million BTU per hour heat input. The steam produced is used in the superphosphoric acid evaporators. No. 6 oil is used as a stand-by fuel, the sulfur content of which is limited by permit conditions at 0.8% maximum.

The combustion gases from boiler "C" and boiler "D" exhaust through a common stack. There is a fabric filter baghouse which is used to control particulate emissions only when COM is fired.

4. Oil fired auxiliary steam boiler "E" is rated at 156 BTU per hour heat input. The steam produced is used to augment the steam produced by the sulfuric acid plants. No. 6 oil is fired, the sulfur content of which is limited by permit conditions at 0.8% maximum.

Emission Evaluation: (1)

Pollutant	Boiler B	Boiler C	Boiler D	Boiler E
Particulates	lb/hr	lb/hr	lb/hr	lb/hr
current	12.01	9.01	9.01	11.55
proposed	14.20	10.65	10.65	13.9
increase	2.19	1.64	1.64	2.35
SO ₂	lb/hr	lb/hr	lb/hr	lb/hr
current	137.16	102.87	102.87	131.88
proposed	174.8	128.58	128.58	170.7
increase	37.64	25.71	25.71	38.82
Fuel Use	GPH	GPH	GPH	GPH
MAX	1092	819	819	1050
AVE	273	210	210	252
COM		922		

(1) AP-42 Emission Factors, Table 1.3.1

The applicant plans to fire No. 6 oil having a sulfur content of 1.0 percent instead of the 0.8 percent maximum presently allowed. The increase in sulfur dioxide emissions, as a result of burning the higher sulfur fuel, exceeds the significant emission rate of 40 tons per year and requires a BACT determination (17-2.500(5) (c)FAC) for the pollutant sulfur dioxide.

The applicant has submitted several applications that require a BACT determination. Three determinations have been made by combining similar sources as follows:

PART I - Sulfuric Acid Plants,
 PART II - Boiler Fuel Conversions
 PART III - DAP Dryer Fuel Conversion.

BACT Determination Requested by the Applicant:

Boilers, B, C, D, and E

Pollutant	Emission Limit
SO ₂ (oil)	1.1 lb/million BTU heat input (1% sulfur content)
SO ₂ (com)	0.9% sulfur content

Date of Receipt of a BACT application:

May 27, 1982

Date of Publication in the Florida Administrative Weekly:

June 11, 1982

Review Group Members:

The final determination was based upon comments received from the New Source Review Section and the Air Modeling Section.

BACT Determined by DER:

Auxiliary boiler E - Swift Creek Complex
Auxiliary boiler B, C, D - Suwannee River Complex

Sulfur dioxide emissions controlled by limiting the sulfur content of the No. 6 oil fired to a maximum of 1.0 percent and the COM fuel to 0.9 percent.

Compliance with the SO₂ emission limit will be based upon the Sulfur content of the fuel fired. Each shipment of fuel delivered to the facility will be sampled and the sulfur content determined and recorded. A certified analysis from the applicants fuel supplier may be substituted for on-site analysis. Applicable test methods by the American Society for Testing Material (A.S.T.M.) will be used.

Justification of DER Determination:

The facility is within 50 kilometers of the Okefenokee National Wilderness area, a Class 1 area. Air modeling indicates that at the conditions determined as BACT, the impact of sulfur dioxide emissions from the facility will be just less than the maximum allowable increase for a Class 1 area.

Details of the Analysis May be Obtained by Contacting:

Edward Palagyi, BACT Coordinator
Department of Environmental Regulation
Bureau of Air Quality Management
2600 Blair Stone Road
Tallahassee, Florida 32301

Recommended By:

AS *Steve Smallwood*
Steve Smallwood, Chief BAQM

Date: 11/2/82

Approved:

Victoria J. Eschinkel
Victoria J. Eschinkel, Secretary

Date: 11/18/82

BEST AVAILABLE CONTROL TECHNOLOGY (BACT) DETERMINATION

PART III OF III

OCCIDENTAL CHEMICAL COMPANY

HAMILTON COUNTY

The applicant plans to increase the sulfur content of the fuel oil fired in the diammonium phosphate plant (DAP) dryer. The dryer is in the Suwannee River complex located near White Springs, Florida. The existing dryer is gas fired with No. 6 residual oil fired only during periods of gas curtailment. The sulfur content of the oil is to be increased to 1.5 percent from the presently permitted maximum of 0.8 percent.

At maximum dryer capacity No. 6 oil is fired at a rate of 246 gallons per hour. SO₂ emissions, at this rate of oil consumption (assume 80% SO₂ absorption), when firing 0.8% and 1.5% sulfur content oil is 6.3 and 11.8 pounds per hour respectively. The increase in SO₂ emissions would be 5.5 pounds per hour.

A Venturi scrubber in series with a packed tail-gas scrubber is used to reduce the air pollutants emitted in the dryer exhaust gases. Sulfur dioxide emissions are reduced by the control system, and, in addition, by reaction with the material being dried.

The applicant has submitted several applications that require a BACT determination. Three determinations have been made by combining similar sources as follows:

PART I - Sulfuric Acid Plants,
PART II - Boiler Fuel Conversions
PART III - DAP Dryer Fuel Conversion.

BACT Determination Requested by the Applicant:

Pollutant	Emission Limit
SO ₂	0.41 lb/ton P ₂ O ₅ input (fuel with 1.5% sulfur)

Date of Receipt of a BACT Application:

May 27, 1982

Date of Publication in the Florida Administrative Weekly:

June 11, 1982

Review Group Members:

The final determination was based upon comments received from the New Source Review Section and the Air Monitoring Section.

BACT Determined by DER:

Diammonium Phosphate Plant No. 2 product rotary dryer.
Suwannee River Chemical Complex

Sulfur dioxide emissions controlled by limiting the sulfur content of the No. 6 oil fired to a maximum of 1.5 percent, and SO₂ emissions to 0.20 lb. SO₂/ton DAP.

The applicant shall prepare a procedure to prevent the unloading of No. 6 oil containing 1.5% sulfur into the tank(s) which contain No. 6 oil having a lower sulfur content. A record will be kept of the amount of 1.5% oil received and the DAP dryer oil consumption rate. The records shall be made available to the department upon request.

Compliance with the SO₂ emission limit will be based upon the sulfur content of the fuel fired. Each shipment of fuel delivered to the facility will be sampled and the sulfur content determined and recorded. A certified analysis from the applicants fuel supplier may be substituted for on-site analysis. Applicable test methods by the American Society for Testing Material (A.S.T.M.) will be used.

Justification of DER Determination:

To reiterate per the BACT determination, Part II, the facility is within 50 kilometers of the Okefenokee National Wilderness area, a Class I area. Air modeling indicates that at the conditions determined as BACT, the impact of sulfur dioxide emissions from the facility will be just less than the maximum allowable increase for a Class I area.

The quantity of controlled SO₂ emissions from the dryer, when firing 1.5% sulfur content oil, is comparable to the amount of uncontrolled SO₂ emissions when firing 1.0% sulfur content oil. Oil is the stand-by fuel for this unit and would be fired only during periods of gas curtailment.

The use of the same grade fuel oil, but with different sulfur contents, will require, at the minimum, two fuel oil storage tanks. The applicant will have to set up a fuel oil handling procedure to prevent the transfer of the higher sulfur content oil to the wrong tank or other sources.


The department has determined, in this case, that the increase in the sulfur content of the oil fired (0.8% to 1.5%) is reasonable.

provided the anticipated 80% reduction in SO₂ emissions is documented.

Details of the Analysis May be Obtained by Contacting:

Edward Palagyi, BACT Coordinator
Department of Environmental Regulation
Bureau of Air Quality Management
2600 Blair Stone Road
Tallahassee, Florida 32301

Recommended By:



10x Steve Smallwood, Chief BAQM

Date: 11/2/82

Approved:



Victoria J. Tschinkel, Secretary

Date: 11/18/82

Best Available Control Technology (BACT) Determination
Part I of III
Occidental Chemical Company
Hamilton County

The applicant plans to increase production from the sulfuric acid plants "E" and "F" located at their fertilizer grade phosphate rock processing facility at the Swift Creek Chemical Complex near White Springs, Florida. The production capacity of each acid plant is to be increased 25 percent to 2500 tons per day of 100% acid. Both acid plants have inherent in the initial design a production rate of 2300 tons per day with no major equipment modifications. It will be necessary to modify the economizer, gas handling and catalyst loading systems to achieve the 2500 tons per day production rate.

Air pollutants emitted from the sulfuric acid plants will be SO₂, NO_x, CO and sulfuric acid mist increasing the annual ambient air burden by 730,26,1, and 27 tons, respectively. Sulfur dioxide and sulfuric acid mist emissions increase exceeds the significant emission rate and requires a Best Available Control Technology determination as set forth in 17-2.500(2)(f), FAC.

The applicant has submitted several applications that require a BACT determination. Three determinations have been made by combining similar sources as follows:

- PART I - Sulfuric Acid Plants,
- PART II - Boiler Fuel Conversions
- PART III - DAP Dryer Fuel Conversion.

BACT Determination Requested by the Applicant:

Sulfuric Acid Plant E and F.

<u>Pollutant</u>	<u>Emission Limit</u>
SO ₂	4.0 lb/ton 100% acid
H ₂ SO ₄ mist	0.15 lb/ton 100% acid

Sulfur dioxide emissions will be controlled by double absorption with catalyst screening and make up every three to five years.

Sulfuric acid mist emissions will be controlled with HV mist eliminators.

Date of Receipt of a BACT application:

May 27, 1982

Date of Publication in the Florida Administrative Weekly:

June 11, 1982

Review Group Members:

The final determination was based upon comments received from the New Source Review Section and the Air Modeling Section.

BACT Determined by DER:

Sulfur dioxide emissions from sulfuric acid plants E and F not to exceed 4 pounds per tons of 100% sulfuric acid produced.

Sulfuric acid mist emissions from sulfuric acid plants E and F not to exceed 0.15 pounds per ton of 100% sulfuric acid produced.

Visible emissions to be less than 10% opacity.

Test methods and procedures per the NSPS, 40 CFR Part 60, Subpart H, Subsections 60.84 and 60.85.

Justification of DER Determination:

Sulfur dioxide and sulfuric acid mist emissions are subject to standards of performance for sulfuric acid plants (40 CFR 60.80) promulgated in 1971. U. S. EPA reviewed the standard in 1979 (44 FR15742) and decided not to change the emission limits.

BACT for the sulfuric acid plants E and F is determined to be equal to New Source Performance Standards (NSPS) for sulfuric acid plants, 40 CFR 60, Subpart H.

Best Available Control Technology (BACT) Determination
Part II of III
Occidental Chemical Company
Hamilton County

The applicant plans to fire a higher sulfur content fuel in four fossil-fuel fired steam generators located at their facilities near White Springs, Florida. Boiler E is at the Swift Creek Complex and boilers B, C, D are at the Suwannee River Complex. The existing sources are as follows.

1. Gas fired auxiliary steam boiler "B" is rated at 160 million BTU per hour heat input. The steam produced is used to augment the steam produced by the sulfuric acid plants B and C. Boiler B is operated at 25% of rated capacity when the sulfuric acid plants are in operation. No. 6 oil is used as a stand-by fuel, the sulfur content of which is limited by permit conditions at 0.8% maximum.

2. Gas fired auxiliary steam boiler "C" is rated at 120 million BTU per hour heat input. The steam produced is used in the superphosphoric acid evaporators. No. 6 oil is used as a stand-by fuel, the sulfur content of which is limited by permit conditions at 0.8% maximum.

Boiler "C" has recently been modified to fire a coal-oil mixture (COM), also a stand-by fuel for this unit. The sulfur content of the COM is limited by permit conditions at 0.7% maximum.

3. Gas fired auxiliary steam boiler "D" is rated at 120 million BTU per hour heat input. The steam produced is used in the superphosphoric acid evaporators. No. 6 oil is used as a stand-by fuel, the sulfur content of which is limited by permit conditions at 0.8% maximum.

The combustion gases from boiler "C" and boiler "D" exhaust through a common stack. There is a fabric filter baghouse which is used to control particulate emissions only when COM is fired.

4. Oil fired auxiliary steam boiler "E" is rated at 156 BTU per hour heat input. The steam produced is used to augment the steam produced by the sulfuric acid plants. No. 6 oil is fired, the sulfur content of which is limited by permit conditions at 0.8% maximum.

Emission Evaluation: (1)

Pollutant	Boiler B	Boiler C	Boiler D	Boiler E
Particulates	lb/hr	lb/hr	lb/hr	lb/hr
current	12.01	9.01	9.01	11.55
proposed	14.20	10.65	10.65	13.9
increase	2.19	1.64	1.64	2.35
SO ₂	lb/hr	lb/hr	lb/hr	lb/hr
current	137.16	102.87	102.87	131.88
proposed	174.8	128.58	128.58	170.7
increase	37.64	25.71	25.71	38.82
Fuel Use	GPH	GPH	GPH	GPH
MAX	1092	819	819	1050
AVE	273	210	210	252
COM		922		

(1) AP-42 Emission Factors, Table 1.3.1

The applicant plans to fire No. 6 oil having a sulfur content of 1.0 percent instead of the 0.8 percent maximum presently allowed. The increase in sulfur dioxide emissions, as a result of burning the higher sulfur fuel, exceeds the significant emission rate of 40 tons per year and requires a BACT determination (17-2.500(5) (c)FAC) for the pollutant sulfur dioxide.

The applicant has submitted several applications that require a BACT determination. Three determinations have been made by combining similar sources as follows:

- PART I - Sulfuric Acid Plants,
- PART II - Boiler Fuel Conversions
- PART III - DAP Dryer Fuel Conversion.

BACT Determination Requested by the Applicant:

Boilers, B, C, D, and E

Pollutant	Emission Limit
SO ₂ (oil)	1.1 lb/million BTU heat input (1% sulfur content)
SO ₂ (com)	0.9% sulfur content

Date of Receipt of a BACT application:

May 27, 1982

Date of Publication in the Florida Administrative Weekly:

June 11, 1982

Review Group Members:

The final determination was based upon comments received from the New Source Review Section and the Air Modeling Section.

BACT Determined by DER:

Auxiliary boiler E - Swift Creek Complex
Auxiliary boiler B, C, D - Suwannee River Complex

Sulfur dioxide emissions controlled by limiting the sulfur content of the No. 6 oil fired to a maximum of 1.0 percent and the COM fuel to 0.9 percent.

Compliance with the SO₂ emission limit will be based upon the Sulfur content of the fuel fired. Each shipment of fuel delivered to the facility will be sampled and the sulfur content determined and recorded. A certified analysis from the applicants fuel supplier may be substituted for on-site analysis. Applicable test methods by the American Society for Testing Material (A.S.T.M.) will be used.

Justification of DER Determination:

The facility is within 50 kilometers of the Okefenokee National Wilderness area, a Class 1 area. Air modeling indicates that at the conditions determined as BACT, the impact of sulfur dioxide emissions from the facility will be just less than the maximum allowable increase for a Class 1 area.

BEST AVAILABLE CONTROL TECHNOLOGY (BACT) DETERMINATION

PART III OF III

OCCIDENTAL CHEMICAL COMPANY

HAMILTON COUNTY

The applicant plans to increase the sulfur content of the fuel oil fired in the diammonium phosphate plant (DAP) dryer. The dryer is in the Suwannee River complex located near White Springs, Florida. The existing dryer is gas fired with No. 6 residual oil fired only during periods of gas curtailment. The sulfur content of the oil is to be increased to 1.5 percent from the presently permitted maximum of 0.8 percent.

At maximum dryer capacity No. 6 oil is fired at a rate of 246 gallons per hour. SO₂ emissions, at this rate of oil consumption (assume 80% SO₂ absorption), when firing 0.8% and 1.5% sulfur content oil is 6.3 and 11.8 pounds per hour respectively. The increase in SO₂ emissions would be 5.5 pounds per hour.

A Venturi scrubber in series with a packed tail-gas scrubber is used to reduce the air pollutants emitted in the dryer exhaust gases. Sulfur dioxide emissions are reduced by the control system, and, in addition, by reaction with the material being dried.

The applicant has submitted several applications that require a BACT determination. Three determinations have been made by combining similar sources as follows:

- PART I - Sulfuric Acid Plants,
- PART II - Boiler Fuel Conversions
- PART III - DAP Dryer Fuel Conversion.

BACT Determination Requested by the Applicant:

Pollutant	Emission Limit
SO ₂	0.41 lb/ton P ₂ O ₅ input (fuel with 1.5% sulfur)

Date of Receipt of a BACT Application:

May 27, 1982

Date of Publication in the Florida Administrative Weekly:

June 11, 1982

Review Group Members:

The final determination was based upon comments received from the New Source Review Section and the Air Monitoring Section.

BACT Determined by DER:

Diammonium Phosphate Plant No. 2 product rotary dryer.
Suwannee River Chemical Complex

Sulfur dioxide emissions controlled by limiting the sulfur content of the No. 6 oil fired to a maximum of 1.5 percent, and SO₂ emissions to 0.20 lb. SO₂/ton DAP.

The applicant shall prepare a procedure to prevent the unloading of No. 6 oil containing 1.5% sulfur into the tank(s) which contain No. 6 oil having a lower sulfur content. A record will be kept of the amount of 1.5% oil received and the DAP dryer oil consumption rate. The records shall be made available to the department upon request.

Compliance with the SO₂ emission limit will be based upon the sulfur content of the fuel fired. Each shipment of fuel delivered to the facility will be sampled and the sulfur content determined and recorded. A certified analysis from the applicants fuel supplier may be substituted for on-site analysis. Applicable test methods by the American Society for Testing Material (A.S.T.M.) will be used.

Justification of DER Determination:

To reiterate per the BACT determination, Part II, the facility is within 50 kilometers of the Okefenokee National Wilderness area, a Class I area. Air modeling indicates that at the conditions determined as BACT, the impact of sulfur dioxide emissions from the facility will be just less than the maximum allowable increase for a Class I area.

The quantity of controlled SO₂ emissions from the dryer, when firing 1.5% sulfur content oil, is comparable to the amount of uncontrolled SO₂ emissions when firing 1.0% sulfur content oil. Oil is the stand-by fuel for this unit and would be fired only during periods of gas curtailment.

The use of the same grade fuel oil, but with different sulfur contents, will require, at the minimum, two fuel oil storage tanks. The applicant will have to set up a fuel oil handling procedure to prevent the transfer of the higher sulfur content oil to the wrong tank or other sources.

The department has determined, in this case, that the increase in the sulfur content of the oil fired (0.8% to 1.5%) is reasonable.

provided the anticipated 80% reduction in SO₂ emissions is documented.

Details of the Analysis May be Obtained by Contacting:

Edward Palagyi, BACT Coordinator
Department of Environmental Regulation
Bureau of Air Quality Management
2600 Blair Stone Road
Tallahassee, Florida 32301

Recommended By:

St. Henry

10x Steve Smallwood, Chief BAQM

Date: 11/2/82

Approved:

Victoria J. Tschinkel

Victoria J. Tschinkel, Secretary

Date: 11/18/82

State of Florida
DEPARTMENT OF ENVIRONMENTAL REGULATION
INTEROFFICE MEMORANDUM

For Routing To District Offices And/Or To Other Than The Addressee		
To: _____	Loctn.: _____	
To: _____	Loctn.: _____	
To: _____	Loctn.: _____	
From: _____	Date: _____	
Reply Optional []	Reply Required []	Info. Only []
Date Due: _____	Date Due: _____	

for
TO: Victoria J. Tschinkel
FROM: Steve Smallwood *Alan January*
DATE: November 18, 1982

RECEIVED
NOV 18 1982
Office of the Secretary

SUBJ: BACT Determination for Occidental Chemical Company

Attached please find 3 BACT determinations for several source modifications located in White Springs, Hamilton County, Florida.

We recommend that you approve and sign the determination, the results of which will be made specific conditions of the construction permit.

EP/ks

SECTION III: AIR POLLUTION SOURCES & CONTROL DEVICES (Other than Incinerators)

A. Raw Materials and Chemicals Used in your Process, if applicable:

Description	Contaminants		Utilization Rate - lbs/hr	Relate to Flow Diagram
	Type	% Wt		
Sulfur	Dust	1-2	136,464*	A
* Maximum utilization rate; this use rate will normally occur when there is an interruption in the normal supply of molten sulfur and the E and F sulfuric acid plants are operating at 100 percent permitted capacity.				

B. Process Rate, if applicable: (See Section V, Item 1)

- Total Process Input Rate (lbs/hr): 83,333 sulfur vatting rate
- Product Weight (lbs/hr): 136,464 maximum reclamation rate of sulfur from a vat.

C. Airborne Contaminants Emitted:

Name of Contaminant	Emission ¹		Allowed Emission ² Rate per Ch. 17-2, F.A.C.	Allowable ³ Emission lbs/hr	Potential Emission ⁴		Relate to Flow Diagram
	Maximum lbs/hr	Actual T/yr			lbs/hr	T/yr	
Fugitive Part. Matter*	9.8	21.3	NA	9.8	97.5	213	B
* These emissions will be generated only when sulfur is being reclaimed from a vat.							

D. Control Devices: (See Section V, Item 4)

Name and Type (Model & Serial No.)	Contaminant	Efficiency	Range of Particles ⁵ Size Collected (in microns)	Basis for Efficiency (Sec. V, It ⁵)
Water Sprays with wetting agent	Sulfur Dust	90	< 75 μm	Estimate

¹See Section V, Item 2.

²Reference applicable emission standards and units (e.g., Section 17-2.05(6) Table II, E. (1), F.A.C. - 0.1 pounds per million BTU heat input)

³Calculated from operating rate and applicable standard

⁴Emission, if source operated without control (See Section V, Item 3)

⁵If Applicable

SECTION V - SUPPLEMENTAL REQUIREMENTS

1. Use Rate

Sulfur will be reclaimed from rail cars in a molten state and pumped to the vats at a rate of 83,333 pounds per hour (1000 tpd).

Sulfur will be reclaimed from the vats and delivered to a sulfur melter at the rate of 136,464 pounds per hour. This is the maximum rate at which sulfur will be consumed in the E and F sulfur acid plants.

2&3. Uncontrolled and Actual Emissions

Activity	Uncontrolled Emission Factor (1) (lb/ton)	Control Efficiency (2) (%)	Sulfur Handling Rate (tph)	Uncontrolled Emissions		Controlled Emissions	
				(lb/hr)	(tpy) (3)	(lb/hr)	(tpy)
Loading Vat (4)	0	--	41.7	0	0	0	0
Traffic	1.00	90	--	69	149	6.9	14.9
Wind Erosion (5)	0	--	--	0	0	0	0
Off-Loading	0.43	90	68.2	29	64	2.9	6.4
TOTAL				98	213	9.8	21.3

(1) EPA 450/3-77-010

(2) EPA 450/3-77-010

(3) Based on 4380 hours per year of activity

(4) Sulfur is in molten form; therefore there will be no significant emissions

(5) Sulfur in vat form is not subject to effects of wind erosion

4. Attachment 2

5. Control Efficiency

Uncontrolled Emissions (V, 2 & 3) - 98.0 lb/hr
 Controlled Emissions (V, 2 & 3) - 9.8 lb/hr

$$\begin{aligned} \text{Efficiency} &= (98.0 - 9.8) \times 100/98.0 \\ &= 90.0\% \end{aligned}$$

6. Attachment 3

7. Attachment 4

8. Attachment 5

REVISED 11/17/82

SHOLTES  KOOGLER

FUGITIVE SULFUR DUST EMISSION ESTIMATES

VATTED SULFUR STORAGE AREA
OCCIDENTAL CHEMICAL COMPANY
HAMILTON CO, FL

ORIGINAL APPLICATION

"Traffic" related emissions from sulfur reclamation activities were assumed to be included in "off-loading" emissions; perhaps erroneously so. To be more conservative, and consistent with the intent of EPA 450/3-77-010, the permit application has been modified to include emissions generated by the rubber tired excavator and the rubber tired front end loader as "traffic" related emissions.

Emissions resulting from discharging the reclaimed sulfur into the sulfur melter were accounted for twice. "Off-loading" emissions, by a front end loader, include emissions generated when the front end loader picks the reclaimed materials up and those generated when the material is discharged; i.e., a complete reclamation cycle. At the Occidental vatted sulfur area, the front end loader will discharge the reclaimed sulfur directly into the sulfur melter; thus, the emissions associated with melter loading are included in "pile off-loading" activities. In the original application, a separate, and duplicate, emission estimate was made for melter loading emissions.

Revised APPLICATION

Traffic - One rubber tired excavator and one rubber tired front end loader operating 24 hours per day, 7 days per week. Maximum annual operating factor will be 0.5.

Sulfur Consumption From Vatted Storage Area - Maximum hourly reclamation rate will be 68.2 tons/hour. Maximum annual reclamation will be 298,716 tons.

Basic Storage Pile Emission Factor - Reference EPA-450/3-77-010. Emission factor for "active" pile is 0.22 pounds of fugitive dust per ton of material exclusive of wind generated emissions. This is for a pile with activity 5 days per week

and 8-12 hours per day. The Occidental storage will, at maximum activity, have activity 24 hours per day, 7 days per week

$$\begin{aligned} \text{Basic Emission Factor} &= \text{BEF (exclusive of wind)} \\ &= 0.22 (7/5) (24/12) \\ &= 0.62 \text{ lb/ton, uncontrolled} \end{aligned}$$

$$\begin{aligned} \text{Basic Emission Factor (loading)} &= 0.62 \times \text{loading emissions as fraction of loading, traffic and off-loading emissions} \\ &= 0.62 (12\% / [12\% + 40\% + 15\%]) \\ &= 0.11 \text{ lb/ton, uncontrolled} \end{aligned}$$

$$\begin{aligned} \text{Basic Emission Factor (traffic)} &= 0.62 (40\% / [12\% + 40\% + 15\%]) \\ &= 0.37 \text{ lb/ton, uncontrolled} \end{aligned}$$

$$\begin{aligned} \text{Basic Emission Factor (off-loading)} &= 0.62 (15\% / [12\% + 40\% + 15\%]) \\ &= 0.14 \text{ lb/ton, uncontrolled} \end{aligned}$$

$$\begin{aligned} \text{Basic Emission Factor (wind)} &= 0, \text{ see rationale in cover letter} \end{aligned}$$

Activity Factors - Reference EPA 450 / 3-77-010, pg 2-35)

K_1 (loading) = 0; sulfur discharged to vat in a molten state, hence emissions will be nil.

K_2 (traffic) = 1.33; a factor of 1.0 is assumed for the front end loader and a factor of 0.33 is assumed for the excavator which will travel one-third or less the distance of the front end loader

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$K_3(\text{load-out}) = 1.5$; a factor of 0.5 is assumed for the excavator which breaks "large" chunks of sulfur from the vat. A factor of 1.0 was assumed for load-out and discharge to the melter by front end loader

Silt Content - Assumed to be 3.0% = 5

PE Index - 99 for north Florida

Duration in Storage - not applicable; see discussion of wind erosion in cover letter

Adjusted Uncontrolled Emission Factors

$$\begin{aligned} \text{Loading into Vat} \\ = 0 \text{ lb/ton} \end{aligned}$$

$$\begin{aligned} \text{Traffic} \\ = \text{BEF}(\text{traffic}) \times K_2 \times (S/1.5) / (\text{PE}/100)^2 \\ = 0.37 (1.33) (3/1.5) / (99/100)^2 \\ = 1.00 \text{ lb/ton} \end{aligned}$$

$$\begin{aligned} \text{Wind} \\ = 0 \text{ lb/ton} \end{aligned}$$

$$\begin{aligned} \text{Off-loading} \\ = \text{BEF}(\text{off-loading}) \times K_3 \times (S/1.5) / (\text{PE}/100)^2 \\ = 0.14 (1.5) (3/1.5) / (99/100)^2 \\ = 0.43 \text{ lb/ton} \end{aligned}$$

Control Technology - "Traffic" related emissions and pile "off-loading" emissions are both associated to the reclamation of sulfur from the vat and the discharge of sulfur into the melter. Control efficiencies for traffic related activities were assumed to be the same as those listed for pile off-loading (EPA 450/3-77-010, pp 2-38 & 39) since explicit control efficiencies are not listed for traffic activities. Control by water sprays alone is reported to be 50 percent. The effectiveness of water sprays with a wetting agent is not addressed for "pile off-loading" activities. For other pile related activities, however, the addition of a wetting agent increases the effectiveness of water sprays to:

- 80-90 percent for loading onto piles,
- 90 percent for movement of pile, and
- 90 percent for wind erosion.

For "traffic" and "off-loading" related emissions the use of a wetting agent in the water spray system was assumed to be 90 percent effective for reducing fugitive emissions.

Controlled Fugitive Sulfur Dust Emission Rate

$$\begin{aligned} \text{Traffic} &= 1.00 \text{ lb/ton} (1 - 0.90) (68.2 \text{ tons/hour}) = 6.82 \text{ lb/hr} \\ \text{Off-loading} &= 0.43 \text{ lb/ton} (1 - 0.90) (68.2 \text{ tons/hour}) = 2.93 \text{ lb/hr} \end{aligned}$$

$$\text{Total} = 9.75 \text{ lb/hour}$$

- or -

$$\begin{aligned} \text{Traffic} &= 1.00 \text{ lb/ton} (1 - 0.9) (298716 \text{ tpy}) / 2000 \text{ lb/ton} = 14.9 \text{ tpy} \\ \text{Off-loading} &= 0.43 \text{ lb/ton} (1 - 0.9) (298716 \text{ tpy}) / 2000 \text{ lb/ton} = 6.4 \text{ tpy} \end{aligned}$$

$$\text{Total} = 21.3 \text{ tons/yr}$$

Loading into Melter - Included in "pile off-loading" emission estimates. See discussion in above sections.

SECTION III: AIR POLLUTION SOURCES & CONTROL DEVICES (Other than Incinerators)

A. Raw Materials and Chemicals Used in your Process, if applicable:

Description	Contaminants		Utilization Rate - lbs/hr	Relate to Flow Diagram
	Type	% Wt		
Sulfur	Dust	1-2	136,464*	A
* Maximum utilization rate; this use rate will normally occur when there is an interruption in the normal supply of molten sulfur and the E and F sulfuric acid plants are operating at 100 percent permitted capacity.				

B. Process Rate, if applicable: (See Section V, Item 1)

- Total Process Input Rate (lbs/hr): 83,333 sulfur vatting rate
- Product Weight (lbs/hr): 136,464 maximum reclamation rate of sulfur from a vat.

C. Airborne Contaminants Emitted:

Name of Contaminant	Emission ¹		Allowed Emission ² Rate per Ch. 17-2, F.A.C.	Allowable ³ Emission lbs/hr	Potential Emission ⁴		Relate to Flow Diagram
	Maximum lbs/hr	Actual T/yr			lbs/hr	T/yr	
Fugitive Part. Matter*	9.8	21.3	NA	9.8	97.5	213	B
* These emissions will be generated only when sulfur is being reclaimed from a vat.							

D. Control Devices: (See Section V, Item 4)

Name and Type (Model & Serial No.)	Contaminant	Efficiency	Range of Particles ⁵ Size Collected (in microns)	Basis for Efficiency (Sec. V, It ⁵)
Water Sprays with wetting agent	Sulfur Dust	90	< 75 µm	Estimate

¹ See Section V, Item 2.

² Reference applicable emission standards and units (e.g., Section 17-2.05(6) Table II, E. (1), F.A.C. - 0.1 pounds per million BTU heat input)

³ Calculated from operating rate and applicable standard

⁴ Emission, if source operated without control (See Section V, Item 3)

⁵ If Applicable

SECTION V - SUPPLEMENTAL REQUIREMENTS

1. Use Rate

Sulfur will be reclaimed from rail cars in a molten state and pumped to the vats at a rate of 83,333 pounds per hour (1000 tpd).

Sulfur will be reclaimed from the vats and delivered to a sulfur melter at the rate of 136,464 pounds per hour. This is the maximum rate at which sulfur will be consumed in the E and F sulfur acid plants.

2&3. Uncontrolled and Actual Emissions

Activity	Uncontrolled Emission Factor (1) (lb/ton)	Control Efficiency (2) (%)	Sulfur Handling Rate (tph)	Uncontrolled Emissions		Controlled Emissions	
				(lb/hr)	(tpy) (3)	(lb/hr)	(tpy)
Loading Vat (4)	0	--	41.7	0	0	0	0
Traffic	1.00	90	--	69	149	6.9	14.9
Wind Erosion (5)	0	--	--	0	0	0	0
Off-Loading	0.43	90	68.2	29	64	2.9	6.4
TOTAL				98	213	9.8	21.3

- (1) EPA 450/3-77-010
- (2) EPA 450/3-77-010
- (3) Based on 4380 hours per year of activity
- (4) Sulfur is in molten form; therefore there will be no significant emissions
- (5) Sulfur in vat form is not subject to effects of wind erosion

4. Attachment 2

5. Control Efficiency

Uncontrolled Emissions (V, 2 & 3) - 98.0 lb/hr
 Controlled Emissions (V, 2 & 3) - 9.8 lb/hr

$$\text{Efficiency} = (98.0 - 9.8) \times 100/98.0$$

$$= 90.0\%$$

6. Attachment 3

7. Attachment 4

8. Attachment 5

No. 0157765

RECEIPT FOR CERTIFIED MAIL

NO INSURANCE COVERAGE PROVIDED—
NOT FOR INTERNATIONAL MAIL
(See Reverse)

RECIPIENT'S NAME		M. P. McArthur
STREET AND NO.		P. O. Box 300
P.O. OFFICE AND ZIP CODE		White Springs, FL
POSTAGE		\$
CERTIFIED FEE		
SPECIAL DELIVERY		
RESTRICTED DELIVERY		
CONSULT POSTMASTER FOR FEES OPTIONAL SERVICES RETURN RECEIPT SERVICE	SHOW TO WHOM AND DATE DELIVERED	
	SHOW TO WHOM, DATE AND ADDRESS OF DELIVERY	
	SHOW TO WHOM AND DATE DELIVERED WITH RESTRICTED DELIVERY	
	SHOW TO WHOM, DATE AND ADDRESS OF DELIVERY WITH RESTRICTED DELIVERY	
TOTAL POSTAGE AND FEES		\$
POSTMARK OR DATE		11/10/82

PS Form 3800, Apr. 1976

PS Form 3811, Jan. 1979

● **SENDER:** Complete items 1, 2, and 3.
Add your address in the "RETURN TO" space on reverse.

1. The following service is requested (check one.)

Show to whom and date delivered.....

Show to whom, date and address of delivery.....

RESTRICTED DELIVERY
Show to whom and date delivered.....

RESTRICTED DELIVERY.
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(CONSULT POSTMASTER FOR FEES)

ARTICLE ADDRESSED TO:
M. P. McArthur
Post Office Box 300
White Springs, FL 32096

3. ARTICLE DESCRIPTION:

REGISTERED NO.	CERTIFIED NO.	INSURED NO.
	0157763	

(Always obtain signature of addressee or agent)

I have received the article described above.

SIGNATURE Addressee Authorized agent

Barbara Rogers

4. DATE OF DELIVERY: 11-10-82

POSTMARK

5. ADDRESS (Complete only if requested)

6. UNABLE TO DELIVER BECAUSE:

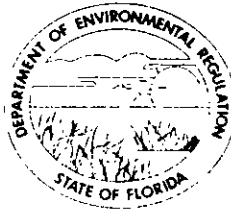
CLERK'S INITIALS
MC

★ GPO : 1979-360-459

RETURN RECEIPT, REGISTERED, INSURED AND CERTIFIED MAIL

STATE OF FLORIDA
DEPARTMENT OF ENVIRONMENTAL REGULATION

TWIN TOWERS OFFICE BUILDING
2600 BLAIR STONE ROAD
TALLAHASSEE, FLORIDA 32301-8241



BOB GRAHAM
GOVERNOR
VICTORIA J. TSCHINKEL
SECRETARY

November 9, 1982

CERTIFIED MAIL - RETURN RECEIPT REQUESTED

Mr. M. P. McArthur
Vice President and General Manager
Occidental Chemical Company
Post Office Box 300
White Springs, Florida 32096

Dear Mr. McArthur:

RE: Preliminary Determination - Occidental Chemical Company
Swift Creek Chemical Complex (AC 24-56209, AC 24-56210,
AC 24-56211 and PSD-FL-082) and Suwannee River Chemical
Complex (AC 24-56212, AC 24-56213, AC 24-56214, AC 24-
56215 and PSD-FL-083)

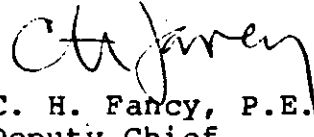
The Florida Department of Environmental Regulation, under the authority delegated by the U.S. Environmental Protection Agency, Region IV, has reviewed your applications to modify the referenced sources under the provisions of the Prevention of Significant Deterioration Regulations (40 CFR 52.21) and has made a preliminary determination of approval with conditions. Please find enclosed one copy of each of the Preliminary Determinations.

Pursuant to Section 403.815, Florida Statutes, and Florida Administrative Code Rule 17-1.62, you are required to publish (at your own expense) the attached Public Notice. The notice must appear, one time only, in the legal ad section of the Lake City Reporter. A copy of the Preliminary Determinations and your applications will be open to public review and comment for a period of 30 days after publication of the notice. The public can also request a public hearing to review and discuss specific issues. At the end of this period, the Department will evaluate the comments received and make a final determination regarding the proposed construction.

Mr. M. P. McArthur
Page Two
November 9, 1982

Should you have questions regarding this information,
please contact Mr. Bill Thomas at (904) 488-1344.

Sincerely,



C. H. Fancy, P.E.
Deputy Chief
Bureau of Air Quality
Management

CHF/pa

Enclosure

cc: Dr. John B. Koogler, Sholtes & Koogler, Environmental
Consultants
Ms. Elisabeth Cummings, U.S. Fish and Wildlife Service
Mr. John Ketteringham, DER Northeast District

Technical Evaluation
and
Preliminary Determination

Occidental Chemical Company
Swift Creek Chemical Complex
Hamilton County, Florida

Permit Numbers

STATE

Sulfuric Acid Plant "F" AC 24-56209
Auxiliary Boiler "E" AC 24-56210
Sulfuric Acid Plant "E" AC 24-56211

FEDERAL

Sulfuric Acid Plant Production Rate Increase PSD-FL-082
and
Auxiliary Boiler "E" Fuel Conversion

Florida Department of Environmental Regulation
Bureau of Air Quality Management
Central Air Permitting

October 25, 1982

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ATTACHMENTS

 Applications to Construct Air Pollutions Sources
 (State and Federal)

 Correspondence

NOTICE OF PROPOSED AGENCY ACTION

The Department of Environmental Regulations gives notice of its intent to issue permits to Occidental Chemical Company. These permits will allow an increase in the production of two existing sulfuric acid plants and the use of fuel oil containing a higher percentage of sulfur than they are currently permitted to use in four existing steam boilers and a diammonium phosphate dryer. These sources are located at the Suwannee River (SRCC) and Swift Creek Chemical Complexes (SCCC) near White Springs in Hamilton County, Florida. No physical modifications to the plant equipment is required to accomplish these operational changes.

*6 objects
+ statement
was changed
to mean
no physical
in order*

A best available control technology (BACT) determination was required for sulfur dioxide (SO₂).

Emission of criteria pollutants from the two chemical complexes will increase by the quantities in tons per year (TPY), listed below.

	SO ₂
SRCC	443.9
SCCC	951

Emissions from the modified sources will consume increment but will not violate any state or federal ambient air quality standards. The maximum increment consumption, in micrograms per cubic meter (ug/m³), and percent of available increment are listed below.

	SRCC		SCCC	
	ug/m ³	Percent	ug/m ³	Percent
SO ₂				
Three hours	256	50	416	81
24-hours	73	80	79	87
Annual	12	60	8	40

A person who is substantially affected by the Department's proposed permitting decision may request a hearing in accordance with Section 120.57, Florida Statutes, and Chapter 17-1 and 28-5 Florida Administrative Code. The request for hearing must be filed (received) in the Office of General Counsel of the Department at 2600 Blair Stone Road, Twin Towers Office Building, Tallahassee, Florida 32301, within (14) days of publication of this notice. Failure to file a request for hearing within this time period shall constitute a waiver of any right such person may have to request hearing under Section 120.57, Florida Statutes.

By authority of the U. S. Environmental Protection Agency, the Florida Department of Environmental Regulation (FDER) has reviewed the proposed construction under Federal Prevention of Significant Deterioration Regulations (40 CFR 52.21). The FDER has made a preliminary determination that the construction can be approved provided certain conditions are met. A summary of the basis for this determination and the application for a permit submitted by Occidental Chemical Company are available for public review in the following FDER offices:

Department of Environmental Regulation
Northeast District
3426 Bills Road
Jacksonville, Florida 32207

Department of Environmental Regulation
2600 Blair Stone Road
Tallahassee, Florida 32301

Columbia County Public Library
490 N. Columbia Street
Lake City, Florida

Any person may send written comments on the proposed action to Mr. Clair Fancy at the Department's Tallahassee address. All comments mailed within 30 days of publication of this notice will be considered in the Department's final determination.

I. SYNOPSIS OF APPLICATION

A. Name and Address of Applicant

Occidental Chemical Company
P. O. Box 300
White Springs, Florida 32096

B. Source Location

The proposed source is located at Occidental Chemical Company's Swift Creek Chemical Complex; at SR 137, White Springs, Hamilton County, Florida. The UTM coordinates are 320.860 km East and 3,369.750 km North.

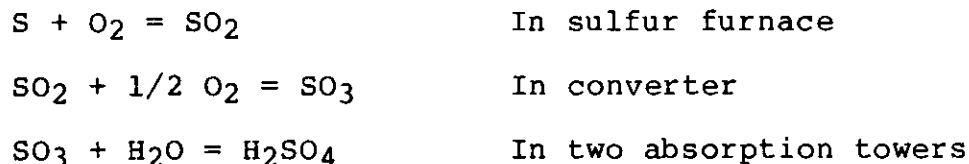
C. Project Description

Occidental proposes to increase the production of sulfuric acid from 2 existing sulfuric acid plants at the Swift Creek Chemical Complex (SCCC) and to increase the sulfur content of the fuel oil used to fire the existing sulfuric acid plants auxiliary boiler.

The proposed production capacity of the two sulfuric acid plants ("E" and "F") will be increased from 2,000 tons per day to 2,500 tons per day each of 100 percent sulfuric acid. The proposed modifications to the "E" auxiliary boiler will result in a change to fuel oil with a maximum of 1.0 percent sulfur and an increase in the annual operating factor from 93.0 to 97.5 percent.

D. Process and Controls

The principal steps in the sulfuric acid manufacturing process consist of burning sulfur (S) in air to form sulfur dioxide (SO₂), combining the sulfur dioxide with oxygen (O₂) to form sulfur trioxide (SO₃), and combining the sulfur trioxide with water (H₂O) to form sulfuric acid (H₂SO₄). The chemical reactions are:



The dual absorption process selected by the applicant is the best demonstrated control technology for SO₂ emissions from sulfuric acid plants. The high efficiency acid mist eliminator is the best demonstrated control technology for acid mist emissions. These controls will reduce the total emissions from the proposed source to a level that is in compliance with the federal New Source Performance Standards (NSPS) requirements of 40 CFR 60, Subpart H.

II. RULE APPLICABILITY

A. Federal Regulations

The proposed project is subject to preconstruction review under federal Prevention of Significant Deterioration (PSD) regulations, Section 52.21 of Title 40 of the Code of Federal Regulations as amended in the Federal Register of August 7, 1980 (45 CFR 52676). Specifically, the proposed project involves three major stationary sources (40 CFR 52.21(b)(1) located in an area currently designed as attainment in accordance with 40 CFR 81.310 for all criteria pollutants regulated under the Clean Air Act (CAA).

The proposed project will be a major modification (40 CFR 52.21(b)(2)) for sulfur dioxide (SO₂), and sulfuric acid mist. Emissions of SO₂ and sulfuric acid mist will increase above the significant criteria set in the PSD regulations. Therefore, the proposed project is subject to PSD review for these pollutants.

The emission rates increases for particulate matter, nitrogen oxides, carbon monoxide and hydrocarbons are below the de minimus levels established for these pollutants.

The PSD review consists of a determination of Best Available Control Technology (BACT) and, unless otherwise exempted, an analysis of the air quality impact of the increased emissions.

The review also includes an analysis of the project's impacts on soils, vegetation and visibility along with air quality impacts resulting from associated commercial, residential and industrial growth.

The proposed project is also subject to the provisions of the federal New Source Performance Standard (NSPS) for sulfuric acid plants (40 CFR 60, Subpart H).

B. State Regulations

The proposed project is subject to preconstruction review under the provisions of Chapter 403, Florida Statutes, and Chapter 17-2, Florida Administrative Code.

The proposed project location, Hamilton County, is an area currently designed as attainment in accordance with Section 17-2.420 FAC for all criteria pollutants.

The sources comprise a major emitting facility for sulfur dioxide (SO₂), sulfuric acid mist and nitrogen oxides (NO_x) as defined in Chapter 17-2, because the potential

emissions of each exceed 100 tons per year (TPY). The project is subject to the provisions of Subsection 17-2.650, FAC, Table II. Emission Limiting Standards, and Subsection 17-2.500 Prevention of Significant Deterioration PSD Review which requires the use of Best Available Control Technology (BACT).

The sources are also subject to the provisions of the federal New Source Performance Standard (NSPS) for sulfuric acid plants, 40 CFR 60, Subpart H. This NSPS has been adopted by reference in Section 17-2.660, FAC.

III. SOURCE IMPACT ANALYSIS

A. Emission Limitations

The regulated pollutant emissions from the two sulfuric acid plants are sulfur dioxide, acid mist and opacity. Organic compounds, nitrogen oxides, nitrosyl sulfuric acid and water vapor may also be present in the emission from the plants.

The operation of the 156 MMBTU/hr auxiliary boiler will produce emissions of particulate matter (PM), sulfur dioxide (SO₂) nitrogen oxides (NO_x), carbon monoxide (CO) and volatile organic compounds (VOC) to the atmosphere.

Table 1 summarizes potential to emit all pollutants regulated under the act which are affected by the proposed project.

As the table shows, the proposed emissions increase of SO₂ and sulfuric acid mist exceeds the significance levels set in the PSD regulations. Although the other regulated pollutants are exempt from a PSD review because their emissions do not increase, they are required to meet all applicable emission limits and standards of performance under the Florida State Implementation Plan.

Best Available Control Technology (BACT) has been determined for SO₂ and sulfuric acid mist for the Sulfuric acid plant and SO₂, for the auxiliary boiler "E". The emission limiting standard selected as BACT and made a condition of the permits are listed in Table 2. Justification for the standards selected is included in Technical Appendix A.

The permitted emission, including those determined as BACT, are in compliance with all applicable requirements of Chapter 17-2 and with New Source Performance Standard (NSPS) requirements of 40 CFR 60, Subpart H.

B. Air Quality Impact Analysis

The air quality impact analysis required for SO₂ and sulfuric acid mist consists of:

- ° An analysis of existing air quality;
- ° A PSD increment analysis (for SO₂ only);
- ° A National and Florida Ambient Air Quality Standards (AAQS) analysis;

Table 1
SUMMARY OF EMISSIONS
(Tons per year)

SOURCE	Pollutant Emissions					
	SO ₂	PM	H ₂ SO ₄ Mist	NO _x	CO	VOC
"E" Sulfuric Acid Plant						
Proposed Emission	1825	--	68.3	64.8	0.5	---
Permitted Emission	1460	--	54.8	51.7	0.4	---
Increase ⁽¹⁾	365	--	13.5	13.1	0.1	---
"F" Sulfuric Acid Plant						
Proposed Emission	1825	--	68.3	64.8	0.5	---
Permitted Emission	1460	--	54.8	51.7	0.4	---
Increase ⁽¹⁾	365	--	13.5	13.1	0.1	---
"E" Auxiliary Boiler						
Proposed Emission	729	59	---	273	23	5
Existing Emission	508	64	---	260	21	4
Increase ⁽¹⁾	221	-5	---	13	2	1
Fugitive Emission ⁽²⁾	----	--	---	<1	1	<1
Net Increase from Proposed Modification	951	-5	27	39.2	3	1
PSD Significance Level ⁽³⁾	40	25	7	40	100	40

(1) Applicant's estimate of emission rate increases that will result from increasing the production capacity of the "E" and "F" sulfuric acid plants from 2,000 TPD to 2,500 TPD each and from increasing the sulfur content of the fuel to the "E" auxiliary boiler to 1.0 percent.

(2) Vehicle Traffic.

(3) 40 CFR 52.21.

Table 2

ALLOWABLE EMISSION LIMITS

SOURCE	POLLUTANT EMISSION							BASIS
	SO ₂	PM	Mist	NO _x	CO	VOC		
"E" Sulfuric Acid Plant Standard	4 lb/ton 100% acid	--	0.15 lb/ton 100% acid	---	---	---	NSPS and BACT	
Emission Rate(lb/hr)	416.7	--	15.6	14.8	0.1	---		
"F" Sulfuric Acid Plant Standard	4 lb/ton 100% acid	--	0.15 lb/ton 100% acid	---	---	---	NSPS and BACT	
Emission Rate(lb/hr)	416.7	--	15.6	14.8	0.1	---		
"E" Auxiliary Boiler Emission Rate	1.1 lb/10 ⁶ BTU heat input and 170.7 lb/hr	-- 13.9	---- ----	---	64	5.3	1.1	BACT and Emission rates as estimated by the applicant

- ° An analysis of impacts on soils, vegetation and visibility and of growth-related air quality impacts; and
- ° A "good engineering practice (GEP)" stack height evaluation.

The analysis of existing air quality generally relies on preconstruction ambient air monitoring data collected in accordance with EPA-approved methods. The PSD increment and AAQS analyses depend on air quality modeling carried out in accordance with EPA guidelines.

Based on these required analyses, the Department has reasonable assurance that the proposed Occidental Chemical Company Swift Creek Chemical Complex (SCCC) modification, as described in this permit and subject to the conditions of approval proposed herein, will not cause or contribute to a violation of any PSD increment or ambient air quality standard. A discussion of the modeling methodology and required analyses follows.

1. Modeling Methodology

Four EPA-approved atmospheric dispersion models were used to predict ground-level pollutant concentrations. The Single-Source (CRSTER) model and the PTMTPW model were used for short-term (24 hours or less) averages to predict maximum concentrations in the vicinity of the facility. CRSTER was used first to establish the meteorological conditions resulting in the highest, second- high impacts. PTMTPW was then run for these days of critical meteorology to further refine the results using all possible sources which may significantly interact with the facility, along with a finer receptor grid spacing (0.1 km).

The Air Quality Display Model (AQDM) was used to predict annual concentrations. Receptors for this modeling were placed at 1.0 km intervals.

The Industrial Source Complex Short-Term (ISCST) model was used to predict short and long term concentrations on the nearest Class I area, the Okefenokee National Wildlife Refuge in southeast Georgia. This model was used to take advantage of the pollutant decay feature written into the program. An SO₂ half-life of 12 hours was used. This additional refinement was needed to show that Class I PSD increments would not be violated.

The surface meteorological data used in the models were National Weather Service (NWS) data collected at Valdosta, Georgia for the period 1972-1976. Upper-air meteorological data were collected at the NWS Waycross, Georgia station for the same period.

Stack parameters and emission rates used in evaluating the proposed modification are given in Tables 1 and 2. Table 1 lists all the SO₂ emission units at both the SCCC and the Suwannee River Chemical Complex (SRCC) facilities at the emission rates to be allowed after the proposed modifications to both facilities. Table 2 lists all SO₂ increment consuming emission units at both facilities for that part of their emission rates which consume increment.

2. Analysis of Existing Air Quality

Under the State regulations (Rule 17-2.500(5)(f)FAC) the applicant is required to submit preconstruction monitoring data for all pollutants for which a significant increase in annual emissions is proposed and for which an ambient air quality standard exists. For the SCCC facility only SO₂ is subject to this rule. (The Department has determined that preconstruction monitoring for sulfuric acid mist is not necessary.) The monitoring must be continuous and in general comprise a one-year period. The Department may reduce the length of this period to no less than four months when sufficient justification warrants. Due to the rural setting of this facility and its remoteness from other SO₂ emitting sources, the Department has determined that four months of continuous monitoring data at one site is sufficient to satisfy the requirement. A similar federal regulation requiring preconstruction monitoring (40 CFR 52.21(m)) is not applicable to the federal permit because a complete application was submitted by the applicant before this regulation went into effect.

The applicant has elected to use an existing monitor operated by the Department to satisfy the monitoring requirement. The monitor is continuous and satisfies the EPA site selection criteria guidelines. Four months of data (April 1982 through July 1982)* have been analysed from this monitor, and are summarized summarized in the following table.

<u>Averaging Period</u>	<u>Highest (ug/m³)</u>	<u>2nd Highest (ug/m³)</u>
1-hour	371	357
3-hour	314	180
24-hour	67	26
4-month	4	

*Monitor began operation April, 1982.

A determination of the background concentration of SO₂ for the area surrounding the SCCC facility can be obtained by averaging the monitored SO₂ values over all hours for which the monitor was not influenced by the SCCC and SRCC sources. This background value is calculated to be 0 ug/m³.

Table 1

SUMMARY OF SULFUR DIOXIDE EMISSIONS
OCCIDENTAL CHEMICAL COMPANY
SRCC & SCCC

SOURCE NAME	EMISSION RATE		STACK HT. (M)	STACK TEMP. (DEG-K)	EXIT VEL. (M/SEC)	STACK DIA. (M)
	LB/HR	(G/SEC)				
Sulfuric Acid A	1208.3	152.25 (1)	61.0	350.0	15.50	1.80
Sulfuric Acid B	1208.3	152.25 (1)	61.0	350.0	15.50	1.80
Sulfuric Acid C	300.0	37.80 (2)	45.7	356.0	28.70	1.59
Sulfuric Acid D	300.0	37.80 (2)	45.7	356.0	28.70	1.59
DAP 1	11.1	1.40 (4)	36.6	322.0	12.20	2.13
DAP 2	11.8	1.49 (4)	42.7	325.0	13.10	2.44
GTSP/Dical	11.1	1.40 (10)	32.3	314.0	13.10	2.13
Auxiliary Boiler A	102.4	12.90 (5)	12.2	466.0	12.50	1.13
Pollyphos Feed Prep.	4.9	0.62 (4)	28.7	342.0	14.90	1.07
Pollyphos Reactor A	5.0	0.63 (6)	30.5	322.0	10.10	1.22
Pollyphos Reactor B	5.0	0.63 (6)	30.5	322.0	10.10	1.22
SPA #1	0.8	0.10 (6)	30.5	318.0	17.80	0.43
Rock Dryer #3 (SCCC)	38.1	4.80 (10)	15.2	317.0	17.20	2.16
Rock Dryer East	28.7	3.61 (10)	18.3	343.0	5.70	2.95
Rock Dryer West	28.7	3.61 (10)	18.3	343.0	5.70	2.95
Auxiliary Boiler B	174.9	22.00 (7)	10.7	468.0	9.50	1.46
Auxiliary Boilers C&D	262.2	33.00 (8)	31.7	468.0	15.20	1.98
Sulfuric Acid E(SCCC)	416.7	52.50 (3)	61.0	356.0	9.30	2.90
Sulfuric Acid F(SCCC)	416.7	52.50 (3)	61.0	356.0	9.30	2.90
Auxiliary Boiler E (SCCC)	170.8	21.50 (4)	15.3	428.0	15.90	1.60

(1) At 1000 tpd 100% H₂SO₄ and 29 lb SO₂/ton of acid.

(2) At 1800 tpd 100% H₂SO₄ and 4 lb SO₂/ton of acid.

(3) At 2500 tpd 100% h₂SO₄ and 4 lb/SO₂/ton of acid.

(4) At 1.5% sulfur fuel and 80% SO₂ sorption.

(5) At 62.5 x 10⁶ BTU/hr and 1.5% sulfur fuel. A 25% operating factor is imposed when Sulfuric Acid Plants A and B are operating at rated capacity.

(6) Based on emission measurements.

(7) At 160 x 10⁶ BTU/hr and 1.0% sulfur fuel.

(8) Two boilers at 120 x 10⁶ BTU/hr each and 1.0% sulfur fuel.

(9) At 156 x 10⁶ BTU/hr and 1.0% sulfur fuel.

(10) Actual emissions with 1.5% sulfur fuel.

Table 2

SUMMARY OF INCREMENT CONSUMING EMISSIONS

<u>Emission Unit</u>	<u>SO₂ Increment Consuming Emission(g/s)</u>
Sulfuric Acid E (SCCC)	52.5
Sulfuric Acid F (SCCC)	52.5
Auxiliary Boiler E (SCCC)	21.5
Auxiliary Boiler B (SRCC)	22.0
Auxiliary Boilers C and D (SRCC)	33.0
DAP 2 "Z"-train (SRCC)	0.69(1)

(1) Only 0.69 g/s of the total SO₂ emission of 1.49 g/s contributes to increment consumption.

3. PSD Increment Analysis

The SCCC facility is located in an area where the Class II PSD increments apply. The nearest Class I area is the Okefenokee National Wildlife Refuge located approximately 40 kilometers to the northeast. Both a Class II and a Class I PSD increment analysis for SO₂ is required.

The emission units at the SCCC facility which consume SO₂ increment are the E and F sulfuric acid plants and the E auxiliary boiler. Increment consuming sources at the SRCC facility have been modeled along with the SCCC sources due to the close proximity of these facilities. No other sources of SO₂ significantly impact this area.

The results of the Class II modeling analysis are contained in the following table.

Pollutant and Time Average	Class II Increment(ug/m ³)	Predicted Increase(ug/m ³)	Percent Increment Consumed
SO ₂			
Three-hour(1)	512	416	81
24-hour(1)	91	79	87
Annual	20	8	40

(1) Not to be exceeded more than once per year.

A more refined modeling analysis was performed to assess the impact of the proposed emission increases on the Okefenokee Class I area. Due to the long distance (approximately 40 km) and, hence the longer transport time of the plume to the Class I area, conversion of some of the SO₂ to sulfates will be realized, thereby lessening the ground-level concentrations of SO₂. The method by which this conversion is simulated in the model is by introducing an appropriate half-life for SO₂--in this case, 12 hours. The results of this modeling analysis are summarized in the following table.

Pollutant and Time Average	Class I Increment(ug/m ³)	Predicted Increase(ug/m ³)	Percent Increment Consumed
SO ₂			
Three-hour(1)	25	25	100
24-hour(1)	5	5	100
Annual	2	1	50

1 Not to be exceeded more than once per year.

No violation of a PSD allowable increment is predicted as a result of the proposed modification at the SCCC facility.

4. AAQS Analysis

An AAQS analysis is required for all pollutants for which a significant increase in annual emissions is proposed. The analysis includes an evaluation of the background concentrations of the subject pollutants and a modeling evaluation of all sources of those pollutants at both the modified facility and any surrounding facilities (within 50 km) which may impact the area.

An evaluation for SO₂ and sulfuric acid mist is required at the SCCC facility. An estimate of the background concentration of SO₂ is obtained from the preconstruction monitoring described in a previous section. A value of 0 ug/m³ for all averaging times is obtained. The maximum ground-level concentrations in the vicinity of the SCCC facility are summarized in the following table.

<u>Pollutant and Time Average</u>	<u>Florida AAQS</u>	<u>National AAQS</u>	<u>Predicted Impact</u>
SO ₂ (ug/m ³)			
Three-hour(1)	1300	1300(2)	425
24-hour(1)	260	365	195
Annual	60	80	10
Sulfuric Acid Mist (ug/m ³)			
Three-hour	-----	-----	11
24-hour	-----	-----	2
Annual	-----	-----	<1

- (1) Not to be exceeded more than once per year
 (2) Secondary Standard.

5. Analysis of Impacts on Soils, Vegetation, and Visibility and Growth-Related Air Quality Impacts

The maximum ground-level concentrations predicted to occur as a result of the proposed modifications at SCCC are below the applicable National and Florida AAQS for SO₂, including the secondary standard designed to protect public welfare-related values. Therefore, no adverse impacts on soils and vegetation are expected.

The SCCC is located within 40 kilometers of a Class I area' however, no adverse impact on visibility is expected. Significant emission increases will be realized for SO₂ only. Visibility degradation is related much more to particulate and nitrogenoxides emissions.

The proposed modification at the SCCC will result in no new jobs. As a result no growth-related air quality impacts will occur.

6. GEP Stack Height Evaluation

Regulations published by EPA in the Federal Register of February 8, 1982, define GEP stack height as the highest of:

1. 65 meters; or
2. The maximum nearby building height plus 1.5 times the building height or width, whichever is less.

While the actual stack height employed can exceed this height, the stack height used in modeling to determine compliance with the AAQS and PSD increments cannot. As seen in Table 1, all stacks at SCCC are less than the GEP limit of 65 meters.

IV. CONCLUSIONS

Based on the review of the data submitted by Occidental Chemical Company for the modification of two double absorption type sulfuric acid plants, and the increase in the sulfur content of the fuel oil in the "E" auxiliary boiler, the FDER concludes that compliance with all applicable federal and State air quality regulations will be achieved provided certain specific conditions are met. The 1% sulfur content in the fuel oil and the NSPS emission limits proposed by the applicant of 4 pounds of sulfur dioxide per ton of 100% acid produced, 0.15 pounds of acid mist per ton of 100% acid produced, and 10 percent opacity have been determined to be the Best Available Control Technology (BACT). The impact of the sulfuric acid plants and auxiliary boiler "E" emissions will not cause or contribute to a violation of any ambient air quality standard or PSD increment.

The FDER therefore proposes that an authorization to construct be issued to Occidental Chemical Company for the proposed sulfuric acid plants "E" and "F" and auxiliary boiler "E" subject to specific conditions to insure compliance with all applicable regulations. Appendix B includes the proposed conditions.

TECHNICAL APPENDIX A
BACT DETERMINATION

Best Available Control Technology (BACT) Determination
Part I of III
Occidental Chemical Company
Hamilton County

The applicant plans to increase production from the sulfuric acid plants "E" and "F" located at their fertilizer grade phosphate rock processing facility at the Swift Creek Chemical Complex near White Springs, Florida. The production capacity of each acid plant is to be increased 25 percent to 2500 tons per day of 100% acid. Both acid plants have inherent in the initial design a production rate of 2300 tons per day with no major equipment modifications. It will be necessary to modify the economizer, gas handling and catalyst loading systems to achieve the 2500 tons per day production rate.

Air pollutants emitted from the sulfuric acid plants will be SO₂, NO_x, CO and sulfuric acid mist increasing the annual ambient air burden by 730, 26, 1, and 27 tons, respectively. Sulfur dioxide and sulfuric acid mist emissions increase exceeds the significant emission rate and requires a Best Available Control Technology determination as set forth in 17-2.500(2)(f), FAC.

The applicant has submitted several applications that require a BACT determination. Three determinations have been made by combining similar sources as follows:

PART I - Sulfuric Acid Plants,
PART II - Boiler Fuel Conversions
PART III - DAP Dryer Fuel Conversion.

BACT Determination Requested by the Applicant:

Sulfuric Acid Plant E and F.

<u>Pollutant</u>	<u>Emission Limit</u>
SO ₂	4.0 lb/ton 100% acid
H ₂ SO ₄ mist	0.15 lb/ton 100% acid

Sulfur dioxide emissions will be controlled by double absorption with catalyst screening and make up every three to five years.

Sulfuric acid mist emissions will be controlled with HV mist eliminators.

Date of Receipt of a BACT application:

May 27, 1982

Date of Publication in the Florida Administrative Weekly:

June 11, 1982

Review Group Members:

The final determination was based upon comments received from the New Source Review Section and the Air Modeling Section.

BACT Determined by DER:

Sulfur dioxide emissions from sulfuric acid plants E and F not to exceed 4 pounds per tons of 100% sulfuric acid produced.

Sulfuric acid mist emissions from sulfuric acid plants E and F not to exceed 0.15 pounds per ton of 100% sulfuric acid produced.

Visible emissions to be less than 10% opacity.

Test methods and procedures per the NSPS, 40 CFR Part 60, Subpart H, Subsections 60.84 and 60.85.

Justification of DER Determination:

Sulfur dioxide and sulfuric acid mist emissions are subject to standards of performance for sulfuric acid plants (40 CFR 60.80) promulgated in 1971. U. S. EPA reviewed the standard in 1979 (44 FR15742) and decided not to change the emission limits.

BACT for the sulfuric acid plants E and F is determined to be equal to New Source Performance Standards (NSPS) for sulfuric acid plants, 40 CFR 60, Subpart H.

Details of the Analysis May be Obtained by Contacting:

Edward Palagyi, BACT Coordinator
Department of Environmental Regulation
Bureau of Air Quality Management
2600 Blair Stone Road
Tallahassee, Florida 32301

Recommended By:

CS
for Steve Smallwood, Chief BAQM

Date: 11/2/82

Approved:

Victoria J. Tschinkel, Secretary

Date: _____

Best Available Control Technology (BACT) Determination
Part II of III
Occidental Chemical Company
Hamilton County

The applicant plans to fire a higher sulfur content fuel in four fossil-fuel fired steam generators located at their facilities near White Springs, Florida. Boiler E is at the Swift Creek Complex and boilers B, C, D are at the Suwannee River Complex. The existing sources are as follows.

1. Gas fired auxiliary steam boiler "B" is rated at 160 million BTU per hour heat input. The steam produced is used to augment the steam produced by the sulfuric acid plants B and C. Boiler B is operated at 25% of rated capacity when the sulfuric acid plants are in operation. No. 6 oil is used as a stand-by fuel, the sulfur content of which is limited by permit conditions at 0.8% maximum.

2. Gas fired auxiliary steam boiler "C" is rated at 120 million BTU per hour heat input. The steam produced is used in the superphosphoric acid evaporators. No. 6 oil is used as a stand-by fuel, the sulfur content of which is limited by permit conditions at 0.8% maximum.

Boiler "C" has recently been modified to fire a coal-oil mixture (COM), also a stand-by fuel for this unit. The sulfur content of the COM is limited by permit conditions at 0.7% maximum.

3. Gas fired auxiliary steam boiler "D" is rated at 120 million BTU per hour heat input. The steam produced is used in the superphosphoric acid evaporators. No. 6 oil is used as a stand-by fuel, the sulfur content of which is limited by permit conditions at 0.8% maximum.

The combustion gases from boiler "C" and boiler "D" exhaust through a common stack. There is a fabric filter baghouse which is used to control particulate emissions only when COM is fired.

4. Oil fired auxiliary steam boiler "E" is rated at 156 BTU per hour heat input. The steam produced is used to augment the steam produced by the sulfuric acid plants. No. 6 oil is fired, the sulfur content of which is limited by permit conditions at 0.8% maximum.

Emission Evaluation: (1)

Pollutant	Boiler B	Boiler C	Boiler D	Boiler E
Particulates	lb/hr	lb/hr	lb/hr	lb/hr
current	12.01	9.01	9.01	11.55
proposed	14.20	10.65	10.65	13.9
increase	2.19	1.64	1.64	2.35
SO ₂	lb/hr	lb/hr	lb/hr	lb/hr
current	137.16	102.87	102.87	131.88
proposed	174.8	128.58	128.58	170.7
increase	37.64	25.71	25.71	38.82
Fuel Use	GPH	GPH	GPH	GPH
MAX	1092	819	819	1050
AVE	273	210	210	252
COM		922		

(1) AP-42 Emission Factors, Table 1.3.1

The applicant plans to fire No. 6 oil having a sulfur content of 1.0 percent instead of the 0.8 percent maximum presently allowed. The increase in sulfur dioxide emissions, as a result of burning the higher sulfur fuel, exceeds the significant emission rate of 40 tons per year and requires a BACT determination (17-2.500(5) (c)FAC) for the pollutant sulfur dioxide.

The applicant has submitted several applications that require a BACT determination. Three determinations have been made by combining similar sources as follows:

- PART I - Sulfuric Acid Plants,
- PART II - Boiler Fuel Conversions
- PART III - DAP Dryer Fuel Conversion.

BACT Determination Requested by the Applicant:

Boilers, B, C, D, and E

Pollutant	Emission Limit
SO ₂ (oil)	1.1 lb/million BTU heat input (1% sulfur content)
SO ₂ (com)	0.9% sulfur content

Date of Receipt of a BACT application:

May 27, 1982

Date of Publication in the Florida Administrative Weekly:

June 11, 1982

Review Group Members:

The final determination was based upon comments received from the New Source Review Section and the Air Modeling Section.

BACT Determined by DER:

Auxiliary boiler E - Swift Creek Complex
Auxiliary boiler B, C, D - Suwannee River Complex

Sulfur dioxide emissions controlled by limiting the sulfur content of the No. 6 oil fired to a maximum of 1.0 percent and the COM fuel to 0.9 percent.

Compliance with the SO₂ emission limit will be based upon the Sulfur content of the fuel fired. Each shipment of fuel delivered to the facility will be sampled and the sulfur content determined and recorded. A certified analysis from the applicants fuel supplier may be substituted for on-site analysis. Applicable test methods by the American Society for Testing Material (A.S.T.M.) will be used.

Justification of DER Determination:

The facility is within 50 kilometers of the Okefenokee National Wilderness area, a Class 1 area. Air modeling indicates that at the conditions determined as BACT, the impact of sulfur dioxide emissions from the facility will be just less than the maximum allowable increase for a Class 1 area.

Details of the Analysis May Be Obtained by Contacting:

Edward Palagyi, BACT Coordinator
Department of Environmental Regulation
Bureau of Air Quality Management
2600 Blair Stone Road
Tallahassee, Florida 32301

Recommended By:


for Steve Smallwood, Chief BAQM

Date: 11/7/82

Approved:

Victoria J. Tschinkel, Secretary

Date: _____

BEST AVAILABLE CONTROL TECHNOLOGY (BACT) DETERMINATION

PART III OF III

OCCIDENTAL CHEMICAL COMPANY

HAMILTON COUNTY

The applicant plans to increase the sulfur content of the fuel oil fired in the diammonium phosphate plant (DAP) dryer. The dryer is in the Suwannee River complex located near White Springs, Florida. The existing dryer is gas fired with No. 6 residual oil fired only during periods of gas curtailment. The sulfur content of the oil is to be increased to 1.5 percent from the presently permitted maximum of 0.8 percent.

At maximum dryer capacity No. 6 oil is fired at a rate of 246 gallons per hour. SO₂ emissions, at this rate of oil consumption (assume 80% SO₂ absorption), when firing 0.8% and 1.5% sulfur content oil is 6.3 and 11.8 pounds per hour respectively. The increase in SO₂ emissions would be 5.5 pounds per hour.

A Venturi scrubber in series with a packed tail-gas scrubber is used to reduce the air pollutants emitted in the dryer exhaust gases. Sulfur dioxide emissions are reduced by the control system, and, in addition, by reaction with the material being dried.

The applicant has submitted several applications that require a BACT determination. Three determinations have been made by combining similar sources as follows:

- PART I - Sulfuric Acid Plants,
- PART II - Boiler Fuel Conversions
- PART III - DAP Dryer Fuel Conversion.

BACT Determination Requested by the Applicant:

Pollutant	Emission Limit
SO ₂	0.41 lb/ton P ₂ O ₅ input (fuel with 1.5% sulfur)

Date of Receipt of a BACT Application:

May 27, 1982

Date of Publication in the Florida Administrative Weekly:

June 11, 1982

Review Group Members:

The final determination was based upon comments received from the New Source Review Section and the Air Monitoring Section.

BACT Determined by DER:

Diammonium Phosphate Plant No. 2 product rotary dryer.
Suwannee River Chemical Complex

Sulfur dioxide emissions controlled by limiting the sulfur content of the No. 6 oil fired to a maximum of 1.5 percent, and SO₂ emissions to 0.20 lb. SO₂/ton DAP.

The applicant shall prepare a procedure to prevent the unloading of No. 6 oil containing 1.5% sulfur into the tank(s) which contain No. 6 oil having a lower sulfur content. A record will be kept of the amount of 1.5% oil received and the DAP dryer oil consumption rate. The records shall be made available to the department upon request.

Compliance with the SO₂ emission limit will be based upon the sulfur content of the fuel fired. Each shipment of fuel delivered to the facility will be sampled and the sulfur content determined and recorded. A certified analysis from the applicants fuel supplier may be substituted for on-site analysis. Applicable test methods by the American Society for Testing Material (A.S.T.M.) will be used.

Justification of DER Determination:

To reiterate per the BACT determination, Part II, the facility is within 50 kilometers of the Okefenokee National Wilderness area, a Class I area. Air modeling indicates that at the conditions determined as BACT, the impact of sulfur dioxide emissions from the facility will be just less than the maximum allowable increase for a Class I area.

The quantity of controlled SO₂ emissions from the dryer, when firing 1.5% sulfur content oil, is comparable to the amount of uncontrolled SO₂ emissions when firing 1.0% sulfur content oil. Oil is the stand-by fuel for this unit and would be fired only during periods of gas curtailment.

The use of the same grade fuel oil, but with different sulfur contents, will require, at the minimum, two fuel oil storage tanks. The applicant will have to set up a fuel oil handling procedure to prevent the transfer of the higher sulfur content oil to the wrong tank or other sources.

The department has determined, in this case, that the increase in the sulfur content of the oil fired (0.8% to 1.5%) is reasonable.

provided the anticipated 80% reduction in SO₂ emissions is documented.

Details of the Analysis May be Obtained by Contacting:

Edward Palagyi, BACT Coordinator
Department of Environmental Regulation
Bureau of Air Quality Management
2600 Blair Stone Road
Tallahassee, Florida 32301

Recommended By:

Ch. Honey

108 Steve Smallwood, Chief BAQM

Date: 11/2/82

Approved:

Victoria J. Tschinkel, Secretary

Date: _____

APPENDIX B

SPECIFIC CONDITIONS

FDER proposes a preliminary determination of approval with conditions for the project requested by Occidental Chemical Company in the permit applications submitted on June 8, 1981 (federal application) and May 21, 1982 (state application).

Special conditions listed in the state permits AC 24-56209, AC 24-56210, AC 24-56211 are adopted as special conditions for the federal permit, PSD-FL-082, for these sources.

The attached General Conditions (federal) are also made a part of the proposed federal permit PSD-FL-082.

Technical Evaluation
and
Preliminary Determination

Occidental Chemical Company
Suwannee River Chemical Complex
Hamilton County, Florida

PERMIT NUMBERS:

STATE

Auxiliary Boiler "B"	AC 24-56212
Auxiliary Boiler "C"	AC 24-56214
Auxiliary Boiler "D"	AC 24-56213
DAP Plant No. 2	AC 24-56215

FEDERAL

SRCC Fuel Conversion Project PSD-FL-083

Florida Department of Environmental Regulation
Bureau of Air Quality Management
Central Air Permitting
October 25, 1982

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 Application to Construct Air Pollution Sources.
 (State and Federal)

 Correspondence

I. SYNOPSIS OF APPLICATION

A. Name and Address of Applicant

Occidental Chemical Company
P. O. Box 300
White Springs, Florida 32096

B. Source Location

Occidental Chemical Company (OCC) operates two phosphate fertilizer facilities north of White Springs in Hamilton County, Florida. The facilities are the Swift Creek Chemical Complex (SCCC), located on SR 100 and the Suwannee River Chemical Complex, (SRCC) located on SR 137. The Department of Environmental Regulation (DER) is currently processing applications for modifications to existing sources at both chemical complexes. This determination is for the modification planned for the SRCC whose UTM coordinates are 328.320 km. East and 3,368.810 km. North. Modifications planned for SCCC are discussed in a separate document.

C. Project Description

The modifications requested by OCC is the substitution of a lower grade No. 6 fuel oil (higher sulfur content) in three auxiliary boilers (B, C, and D) and the No. 2 DAP plant dryer. The maximum sulfur content of the fuel oil used in the boilers will be increased from 0.8 to 1.0 percent. In the No. 2 DAP plant, the maximum sulfur in the fuel oil will increase from 0.8 to 1.5 percent.

No physical changes are required for this equipment to burn the lower grade fuel oil. The lower grade fuel will increase sulfur dioxide emissions from these units. The maximum sulfur content of the fuels is such that no violations of federal or state regulations will be caused by its use.

D. Process Description

Auxiliary boiler "B" produces 125,000 pounds of steam per hour from 160 MMBTU/hour heat input. It can use either natural gas or No. 6 oil for fuel. The 160 MMBTU/hour heat input is equivalent to 1,067 GPH of No. 6 fuel oil. The steam from auxiliary boiler B is used to augment steam produced by two sulfuric acid plants, B and C.

Auxiliary boiler "D" produces 100,000 pounds of steam per hour from 120 MMBTU/hour heat input. It can use either natural gas or No. 6 oil fuel. The 120 MMBTU/hour heat input is equivalent to 820 GPH No. 6 fuel oil. The steam

from auxiliary boiler D is used in the superphosphoric acid plant. This boiler shares a common stack with auxiliary boiler C.

Auxiliary boiler "C" is identical to auxiliary boiler D except it has been modified to allow the use of COM fuel also. A baghouse and dust collector are needed when COM fuel is burned in this boiler to control particulate matter emissions.

The dryer in the No. 2 DAP plant uses 36 MMBTU/hour of natural gas or No. 6 oil as fuel to produce 60 TPH DAP product. This requires 248 GPH of oil. OCC reports over 80 percent of the sulfur dioxide produced when the sulfur in the oil is burned is retained in the product and not emitted to the atmosphere. The free ammonia in the scrubber reacts with the sulfur dioxide and this compound is removed by the acid scrubbing liquid, which is later neutralized to form DAP.

II. RULE APPLICABILITY

A. Federal Regulations

The proposed project, substituting fuel oil with a maximum sulfur content of 1.0 percent in boilers B, C, and D and 1.5 percent for the No. 2 DAP plant for the 0.8 percent the sources are presently permitted to burn, is subject to preconstruction review under federal prevention of significant deterioration (PSD) regulations, Section 52.21 of Title 40 of the Code of Federal Regulations (40 CFR 52.21) as amended in the Federal Register of August 7, 1980 (45 FR 52676). Specifically, each modified boiler and the No. 2 DAP plant constitute a major stationary source (40 CFR 52.21(b)(1)) located in an area designated in 40 CFR 81.310 as attainment for all criteria pollutants.

Use of the alternate fuels will result in a significant net emission increase of sulfur dioxide, thereby rendering it a major modification (40 CFR 52.21 (b)(2)) subject to PSD review (40 CFR 52.21(i)). The increase in emissions of other criteria pollutants are below the significant levels.

Full PSD review is required for each pollutant for which a significant net emission increase would occur. For this modification, the review is required for sulfur dioxide. The review consists of a determination of best available control technology (BACT) and an analysis of the air quality impact of the increased emissions. The review also includes an analysis of the impact of the proposed project on soils, vegetation, visibility and the air quality impact resulting from associated commercial, residential and industrial growth.

B. State Regulations

The proposed project, increasing the sulfur content of the fuel oil used in boilers B, C, and D and the No. 2 DAP plant, is subject to preconstruction review under the provisions of Chapter 403, FS, and Chapter 17-2, FAC.

The plant site is in an area designated attainment for all criteria pollutants. It is within 40 km of the Okefenokee National Wilderness Refuge, a Class I area.

The plant is a major emitting facility for sulfur dioxide, nitrogen oxides, and particulate matter as defined in Chapter 17-2 because the potential emissions of each of these criteria pollutants exceeds 100 TPY.

The project is subject to the provisions of Subsection 17-2.500, Prevention of Significant Deterioration (PSD),

because the modification will result in increased emissions of sulfur dioxide above the significant levels listed in Table 500-2, Regulated Air Pollutants - Significant Emission Rates.

PSD requires the use of Best Available Control Technology (BACT), determination of the ambient air impact and preconstruction air quality monitoring and analysis.

III. SOURCE IMPACT ANALYSIS

A. Emission Limitations

The modification to the three (3) auxiliary boilers and DAP dryer will produce emissions of particulate matter (PM), sulfur dioxide (SO₂), nitrogen oxides (NO_x), carbon monoxide (CO) and volatile organic compounds (VOC) to the atmosphere.

Table 1 summarizes potential to emit all pollutants regulated under the act which are affected by the proposed project.

As the table shows, the proposed emissions increase of SO₂ exceeds the significance levels set in the PSD regulations. Although the other regulated pollutants are exempt from a PSD review because their emissions do not increase, they are required to meet all applicable emission limits and standards of performance under the Florida State Implementation Plan.

Best Available Control Technology (BACT) has been determined for SO₂.

The emission limiting standard selected as BACT and made a condition of the permits are listed in Table 2. Justification for the standards selected is included in Technical Appendix A.

The permitted emission, including those determined as BACT, are in compliance with all applicable requirements of Chapter 17-2 and Federal regulations 40 CFR 52.21.

B. Air Quality Impact Analysis

The air quality impact analysis required for SO₂ consists of:

- ° An analysis of existing air quality;
- ° A PSD increment analysis;
- ° A National and Florida Ambient Air Quality Standards (AAQS) analysis;
- ° An analysis of impacts on soils, vegetation and visibility and of growth-related air quality impacts; and
- ° A "good engineering practice (GEP)" stack height evaluation.

Table 1

SUMMARY OF EMISSIONS

(Tons per year)⁽¹⁾

SOURCE	POLLUTANT				
	PM	SO ₂	NO ₂	CO	VOC
Boiler "B"					
Permitted ⁽²⁾					
Proposed ⁽³⁾	70.00	597		---	---
Increase	62.3	765.8	287.2	23.9	4.8
	-7.7	168.8		-0-	-0-
Boiler "C"					
Permitted ⁽²⁾					
Proposed ⁽³⁾	39.5	442.4	----	----	----
Increase	16.6	572.1	239	18.4	4.5
	22.9	129.7	-0-	-0-	-0-
Boiler "D"					
Permitted ⁽²⁾					
Proposed ⁽³⁾	39.5	442.4	----	----	----
Increase	46.7	564.0	215	18	4
	7.2	121.6	-0-	-0-	-0-
TOTAL INCREASE**	22.4	420.1	-0-	-0-	-0-
#2 DAP Dryer*	PM	SO ₂	F		
Permitted ⁽²⁾	193	27.7	6.1	---	---
Proposed ⁽³⁾	193	51.5	6.1	---	---
Increase	----	23.8	-0-	---	---
TOTAL INCREASE**	-0-	23.8	-0-	-0-	-0-
Significant Levels	25	40	40	3	100
					40

(1) Emissions calculations based on 8760 hours per year and 100% on oil for Boilers B,D and DAP plant No. 2. Boiler C calculations are based on 100% on COM.

(2) Permitted emissions as stated in the federal application PSD-FL-083 (Table 2-1) and Boiler B operating permit AO 24-34186
Boiler C and D operating permit AO 24-21059, and
DAP plant #2 operating permit AO 24-33051

(3) Proposed emissions as calculated by the applicant in the State applications and additional correspondence

* Fluoride Emissions for the #2 DAP plant will not change (0.06#F/TP₂O₅)

** Emission rate increases of regulated pollutants (nitrogen oxides, VOC and carbon monoxide) will not be affected by the proposed change.

Table 2

ALLOWABLE EMISSIONS

SOURCE/FUEL	PM		SO ₂		NOx		CO		VOC	
	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
Boiler B Oil ⁽²⁾	14.2	62.3	174.8	765.8	65.5	287.2	5.5	23.9	1.1	4.8
This boiler shall be allowed to operate 60% of rated capacity (Specific Condition No. 1).										
Boiler C*										
Gas	1.2	5.3	0.1	0.3	21.0	92.0	2.0	8.9	0.4	1.6
Oil ⁽²⁾	10.7	46.7	128.7	563.9	49.2	215.5	4.1	18.0	0.8	3.6
COM ⁽³⁾	3.8	16.6	130.6	572.1	54.6	239.2	4.2	18.4	1.0	4.5
Boiler D*										
Gas	1.2	5.3	0.1	0.3	21.0	92.0	2.0	9	0.4	2
Oil	10.7	47	128.7	564	49.2	215	4.1	18	0.8	4
#2 DAP Dryer Oil ⁽⁴⁾	46	193	11.8	51.5						

- (1) Allowable Emissions as estimated by the applicant based on an operating time of 8760 hours per year with the exceptions as noted in this table.
- (2) SO₂ emission limit shall not exceed 1.1 lb/MMBTU heat input (Fuel oil with 1% sulfur content).
- (3) Coal-Oil mix (COM) with 0.9% sulfur content.
- (4) Fuel oil with 1.5% sulfur content. (SO₂ emission limit shall not exceed 0.2 lb/ton DAP).

Fluoride emissions shall not exceed 1.74 lb/hr and 0.6#F/TP₂₀₅.

Boilers C, and D shall be allowed to operate 25% of the time.

*Boiler "C" shares a common stack with auxiliary boiler "D".

The analysis of existing air quality generally relies on preconstruction ambient air monitoring data collected in accordance with EPA-approved methods. The PSD increment and AAQS analyses depend on air quality modeling carried out in accordance with EPA guidelines.

Based on these required analyses, the department has reasonable assurance that the proposed Occidental Chemical Company Suwannee River Chemical Complex (SRCC) modification, as described in this permit and subject to the conditions of approval proposed herein, will not cause or contribute to a violation of any PSD increment or ambient air quality standard. A discussion of the modeling methodology and required analyses follows.

1. Modeling Methodology

Four EPA-approved atmospheric dispersion models were used to predict ground-level pollutant concentrations. The Single-Source (CRSTER) model and the PTMTPW model were used for short-term (24 hours or less) averages to predict maximum concentrations in the vicinity of the facility. CRSTER was used first to establish the meteorological conditions resulting in the highest, second-high impacts. PTMTPW was then run for these days of critical meteorology to further refine the results using all possible sources which may significantly interact with the facility, along with a finer receptor grid spacing (0.1 km).

The Industrial Source Complex Long-Term (ISCLT) was used to predict annual concentrations. Receptors for this modeling were placed at 0.25 km intervals.

The Industrial Source Complex Short-Term (ISCST) model was used to predict short- and long-term concentrations on the nearest Class I area, the Okefenokee National Wildlife Refuge in southeast Georgia. This model was used to take advantage of the pollutant decay feature written into the program. An SO₂ half-life of 12 hours was used. This additional refinement was needed to show that Class I PSD increments would not be violated.

The surface meteorological data used in the models were National Weather Service (NWS) data collected at Valdosta, Georgia for the period 1972-1976. Upper-air meteorological data were collected at the NWS Waycross, Georgia station for the same period.

Stack parameters and emission rates used in evaluating the proposed modification are given in Tables 1 and 2. Table 1 lists all the SO₂ emission units at both the SRCC and the Swift Creek Chemical Complex (SCCC) facilities at the emission rates to be allowed after the proposed modifications to both facilities. Table 2 lists all SO₂ increment consuming emission units at

both facilities for that part of their emission rates which consume increment.

2. Analysis of Existing Air Quality

Under the State regulations (Rule 17-2.500(5)(f), FAC) the applicant is required to submit preconstruction monitoring data for all pollutants for which a significant increase in annual emissions is proposed and for which an ambient air quality standard exists. For the SRCC facility only SO₂ is subject to this rule. The monitoring must be continuous and in general comprise a one-year period. The Department may reduce the length of this period to no less than four months when sufficient justification warrants. Due to the rural setting of this facility and its remoteness from other SO₂ emitting sources, the Department has determined that four months of continuous monitoring data at one site is sufficient to satisfy the requirement. A similar federal regulation requiring preconstruction monitoring (40 CFR 52.21(m)) is not applicable to the federal permit because a complete application was submitted by the applicant before this regulation went into effect.

The applicant has elected to use an existing monitor operated by the Department to satisfy the monitoring requirement. The monitor is continuous and satisfies the EPA site selection criteria guidelines. Four months of data (April 1982 through July 1982)* have been analysed from this monitor, and are summarized in the following table.

<u>Averaging Period</u>	<u>Highest (ug/m³)</u>	<u>2nd Highest (ug/m³)</u>
1-hour	371	357
3-hour	314	180
24-hour	67	26
4-month	4	

*Monitor began operation April, 1982.

A determination of the background concentration of SO₂ for the area surrounding the SRCC facility can be obtained by averaging the monitored SO₂ values over all hours for which the monitor was not influenced by the SRCC and SCCC sources. This background value is calculated to be 0 ug/m³.

Table 1

SUMMARY OF SULFUR DIOXIDE EMISSIONS
OCCIDENTAL CHEMICAL COMPANY
SRCC & SCCC

SOURCE NAME	EMISSION RATE		STACK HT. (M)	STACK TEMP. (DEG-K)	EXIT VEL. (M/SEC)	STACK DIA. (M)
	LB/HR	(G/SEC)				
Sulfuric Acid A	1208.3	152.25 (1)	61.0	350.0	15.50	1.80
Sulfuric Acid B	1208.3	152.25 (1)	61.0	350.0	15.50	1.80
Sulfuric Acid C	300.0	37.80 (2)	45.7	356.0	28.70	1.59
Sulfuric Acid D	300.0	37.80 (2)	45.7	356.0	28.70	1.59
DAP 1	11.1	1.40 (4)	36.6	322.0	12.20	2.13
DAP 2	11.8	1.49 (4)	42.7	325.0	13.10	2.44
GTSP/Dical	11.1	1.40 (10)	32.3	314.0	13.10	2.13
Auxiliary Boiler A	102.4	12.90 (5)	12.2	466.0	12.50	1.13
Pollyphos Feed Prep.	4.9	0.62 (4)	28.7	342.0	14.90	1.07
Pollyphos Reactor A	5.0	0.63 (6)	30.5	322.0	10.10	1.22
Pollyphos Reactor B	5.0	0.63 (6)	30.5	322.0	10.10	1.22
SPA #1	0.8	0.10 (6)	30.5	318.0	17.80	0.43
Rock Dryer #3 (SCCC)	38.1	4.80 (10)	15.2	317.0	17.20	2.16
Rock Dryer East	28.7	3.61 (10)	18.3	343.0	5.70	2.95
Rock Dryer West	28.7	3.61 (10)	18.3	343.0	5.70	2.95
Auxiliary Boiler B	174.9	22.00 (7)	10.7	468.0	9.50	1.46
Auxiliary Boilers C&D	262.2	33.00 (8)	31.7	468.0	15.20	1.98
Sulfuric Acid E(SCCC)	416.7	52.50 (3)	61.0	356.0	9.30	2.90
Sulfuric Acid F(SCCC)	416.7	52.50 (3)	61.0	356.0	9.30	2.90
Auxiliary Boiler E (SCCC)	170.8	21.50 (4)	15.3	428.0	15.90	1.60

- (1) At 1000 tpd 100% H₂SO₄ and 29 lb SO₂/ton of acid.
(2) At 1800 tpd 100% H₂SO₄ and 4 lb SO₂/ton of acid.
(3) At 2500 tpd 100% h₂SO₄ and 4 lb/SO₂/ton of acid.
(4) At 1.5% sulfur fuel and 80% SO₂ sorption.
(5) At 62.5 x 10⁶ BTU/hr and 1.5% sulfur fuel. A 25% operating factor is imposed when Sulfuric Acid Plants A and B are operating at rated capacity.
(6) Based on emission measurements.
(7) At 160 x 10⁶ BTU/hr and 1.0% sulfur fuel.
(8) Two boilers at 120 x 10⁶ BTU/hr each and 1.0% sulfur fuel.
(9) At 156 x 10⁶ BTU/hr and 1.0% sulfur fuel.
(10) Actual emissions with 1.5% sulfur fuel.

Table 2

SUMMARY OF INCREMENT CONSUMING EMISSIONS

<u>Emission Unit</u>	<u>SO₂ Increment Consuming Emission(g/s)</u>
Sulfuric Acid E (SCCC)	52.5
Sulfuric Acid F (SCCC)	52.5
Auxiliary Boiler E (SCCC)	21.5
Auxiliary Boiler B (SRCC)	22.0
Auxiliary Boilers C and D (SRCC)	33.0
<u>DAP 2 "Z"-train (SRCC)</u>	<u>0.69(1)</u>

(1) Only 0.69 g/s of the total emission rate of 1.49 g/s contributes to increment consumption.

3. PSD Increment Analysis

The SRCC facility is located in an area where the Class II PSD increments apply. The nearest Class I area is the Okefenokee National Wildlife Refuge located approximately 40 kilometers to the northeast. Both a Class II and a Class I PSD increment analysis for SO₂ is required.

The consumption of increment in the area of the SRCC facility is affected by all of the SO₂ emissions from the B, C, and D auxiliary boilers, and by a portion of the SO₂ emissions from the DAP No. 2 "Z"-train. In addition, sources at Occidentals SCCC facility are included because of its close proximity to the SRCC site. No other sources of SO₂ significantly impact this area.

The results of the Class II modeling analysis are summarized in the following table.

Pollutant and Time Average	Class II Increment(ug/m ³)	Predicted Increase(ug/m ³)	Percent Increment Consumed
SO ₂			
Three-hour(1)	512	256	50
24-hour(1)	91	73	80
Annual	20	12	60

1 Not to be exceeded more than once per year.

A more refined modeling analysis was performed to assess the impact of the proposed emission increases on the Okefenokee National Wilderness Refuge Class I area. Due to the long distance (approximately 40 km) and, hence, the longer transport time of the plume to the Class I area, conversion of some of the SO₂ to sulfates will be realized. Predicted ground-level impacts of SO₂ will be lessened depending upon the efficiency of this conversion. The method by which this conversion is simulated in the model is through the introduction of an appropriate SO₂ half-life--in this case, 12 hours.

The results of this modeling analysis are summarized in the following table.

Pollutant and Time Average	Class I Increment(ug/m ³)	Predicted Increase(ug/m ³)	Percent Increment Consumed
SO ₂			
Three-hour(1)	25	25	100
24-hour(1)	5	5	100
Annual	2	1	50

(1) Not to be exceeded more than once per year.

No violation of a PSD allowable increment is predicted as a result of the proposed modification at the SRCC facility.

4. AAQS Analysis

An AAQS analysis is required for all pollutants for which a significant increase in annual emissions is proposed. The analysis includes an evaluation of the background concentration for each applicable pollutant, to take into account distant and natural sources, in addition to the explicit modeling of all sources in the surrounding (within 50 km) area.

An evaluation for SO₂ is required at the SRCC facility. An estimate of the background concentration as obtained from pre-construction monitoring and applicable to all averaging times is 0 ug/m³. The maximum ground-level concentrations in the vicinity of the facility are summarized in the following table.

<u>Pollutant and Time Average</u>	<u>Florida AAQS(ug/m³)</u>	<u>National AAQS(ug/m³)</u>	<u>Predicted Impact(ug/m³)</u>
SO ₂			
Three-hour(1)	1300	1300(2)	425
24-hour(1)	260	365	195
Annual	60	80	10

(1) Not to be exceeded more than once per year

(2) Secondary standard.

5. Analysis of Impacts on Soils, Vegetation, and Visibility and Growth-Related Air Quality Impacts

The maximum ground-level concentrations predicted to occur as a result of the proposed modifications at SRCC are below the applicable National and Florida AAQS for SO₂, including the secondary standard designed to protect public welfare-related values. Therefore, no adverse impacts on soils and vegetation are expected.

The SRCC is located within 40 kilometers of a Class I area; however, no adverse impact on visibility is expected. Significant emission increases will be realized for SO₂ only. Visibility

degradation is related much more to particulate and nitrogenoxides emissions.

The proposed modification at the SRCC will result in no new jobs. As a result no growth-related air quality impacts will occur.

6. GEP Stack Height Evaluation

Regulations published by EPA in the Federal Register of February 8, 1982, define GEP stack height as the highest of:

1. 65 meters; or
2. The maximum nearby building height plus 1.5 times the building height or width, whichever is less.

While the actual stack height employed can exceed this height, the stack height used in modeling to determine compliance with the AAQS and PSD increments cannot. As seen in Table 1, all stacks at SRCC are less than the GEP limit of 65 meters.

IV. CONCLUSION

Based on a review of the data submitted by OCC for increasing the maximum sulfur content of the fuel for the No. 2 DAP plant and auxiliary boilers B, C, and D, the FDER concludes that compliance with all applicable federal and state air quality regulations will be achieved provided certain specific conditions are met. Use of fuel oil containing 1.5 percent sulfur in the No. 2 DAP plant, 1.0 percent sulfur in auxiliary boilers B, C, and D and COM fuel with 0.9 percent sulfur in auxiliary boiler C have been determined to be the Best Available Control Technology (BACT). The impact of the DAP dryer and auxiliary boilers emissions will not cause or contribute to a violation of any ambient air quality standard or PSD increment.

The FDER therefore proposes that an authorization to construct be issued to Occidental Chemical Company for the proposed DAP dryer and auxiliary boilers B, C, and D, subject to specific conditions to insure compliance with all applicable regulations. Appendix B includes the proposed conditions.

Appendix A

BACT DETERMINATION

Best Available Control Technology (BACT) Determination
Part I of III
Occidental Chemical Company
Hamilton County

The applicant plans to increase production from the sulfuric acid plants "E" and "F" located at their fertilizer grade phosphate rock processing facility at the Swift Creek Chemical Complex near White Springs, Florida. The production capacity of each acid plant is to be increased 25 percent to 2500 tons per day of 100% acid. Both acid plants have inherent in the initial design a production rate of 2300 tons per day with no major equipment modifications. It will be necessary to modify the economizer, gas handling and catalyst loading systems to achieve the 2500 tons per day production rate.

Air pollutants emitted from the sulfuric acid plants will be SO₂, NO_x, CO and sulfuric acid mist increasing the annual ambient air burden by 730,26,1, and 27 tons, respectively. Sulfur dioxide and sulfuric acid mist emissions increase exceeds the significant emission rate and requires a Best Available Control Technology determination as set forth in 17-2.500(2)(f), FAC.

The applicant has submitted several applications that require a BACT determination. Three determinations have been made by combining similar sources as follows:

- PART I - Sulfuric Acid Plants,
- PART II - Boiler Fuel Conversions
- PART III - DAP Dryer Fuel Conversion.

BACT Determination Requested by the Applicant:

Sulfuric Acid Plant E and F.

<u>Pollutant</u>	<u>Emission Limit</u>
SO ₂	4.0 lb/ton 100% acid
H ₂ SO ₄ mist	0.15 lb/ton 100% acid

Sulfur dioxide emissions will be controlled by double absorption with catalyst screening and make up every three to five years.

Sulfuric acid mist emissions will be controlled with HV mist eliminators.

Date of Receipt of a BACT application:

May 27, 1982

Date of Publication in the Florida Administrative Weekly:

June 11, 1982

Review Group Members:

The final determination was based upon comments received from the New Source Review Section and the Air Modeling Section.

BACT Determined by DER:

Sulfur dioxide emissions from sulfuric acid plants E and F not to exceed 4 pounds per tons of 100% sulfuric acid produced.

Sulfuric acid mist emissions from sulfuric acid plants E and F not to exceed 0.15 pounds per ton of 100% sulfuric acid produced.

Visible emissions to be less than 10% opacity.

Test methods and procedures per the NSPS, 40 CFR Part 60, Subpart H, Subsections 60.84 and 60.85.

Justification of DER Determination:

Sulfur dioxide and sulfuric acid mist emissions are subject to standards of performance for sulfuric acid plants (40 CFR 60.80) promulgated in 1971. U. S. EPA reviewed the standard in 1979 (44 FR15742) and decided not to change the emission limits.

BACT for the sulfuric acid plants E and F is determined to be equal to New Source Performance Standards (NSPS) for sulfuric acid plants, 40 CFR 60, Subpart H.

Details of the Analysis May be Obtained by Contacting:

Edward Palagyi, BACT Coordinator
Department of Environmental Regulation
Bureau of Air Quality Management
2600 Blair Stone Road
Tallahassee, Florida 32301

Recommended By:

for Steve Smallwood, Chief BAQM

Date: 11/2/82

Approved:

Victoria J. Tschinkel, Secretary

Date: _____

Best Available Control Technology (BACT) Determination
Part II of III
Occidental Chemical Company
Hamilton County

The applicant plans to fire a higher sulfur content fuel in four fossil-fuel fired steam generators located at their facilities near White Springs, Florida. Boiler E is at the Swift Creek Complex and boilers B, C, D are at the Suwannee River Complex. The existing sources are as follows.

1. Gas fired auxiliary steam boiler "B" is rated at 160 million BTU per hour heat input. The steam produced is used to augment the steam produced by the sulfuric acid plants B and C. Boiler B is operated at 25% of rated capacity when the sulfuric acid plants are in operation. No. 6 oil is used as a stand-by fuel, the sulfur content of which is limited by permit conditions at 0.8% maximum.

2. Gas fired auxiliary steam boiler "C" is rated at 120 million BTU per hour heat input. The steam produced is used in the superphosphoric acid evaporators. No. 6 oil is used as a stand-by fuel, the sulfur content of which is limited by permit conditions at 0.8% maximum.

Boiler "C" has recently been modified to fire a coal-oil mixture (COM), also a stand-by fuel for this unit. The sulfur content of the COM is limited by permit conditions at 0.7% maximum.

3. Gas fired auxiliary steam boiler "D" is rated at 120 million BTU per hour heat input. The steam produced is used in the superphosphoric acid evaporators. No. 6 oil is used as a stand-by fuel, the sulfur content of which is limited by permit conditions at 0.8% maximum.

The combustion gases from boiler "C" and boiler "D" exhaust through a common stack. There is a fabric filter baghouse which is used to control particulate emissions only when COM is fired.

4. Oil fired auxiliary steam boiler "E" is rated at 156 BTU per hour heat input. The steam produced is used to augment the steam produced by the sulfuric acid plants. No. 6 oil is fired, the sulfur content of which is limited by permit conditions at 0.8% maximum.

Emission Evaluation: (1)

Pollutant	Boiler B	Boiler C	Boiler D	Boiler E
Particulates	lb/hr	lb/hr	lb/hr	lb/hr
current	12.01	9.01	9.01	11.55
proposed	14.20	10.65	10.65	13.9
increase	2.19	1.64	1.64	2.35
SO ₂	lb/hr	lb/hr	lb/hr	lb/hr
current	137.16	102.87	102.87	131.88
proposed	174.8	128.58	128.58	170.7
increase	37.64	25.71	25.71	38.82
Fuel Use	GPH	GPH	GPH	GPH
MAX	1092	819	819	1050
AVE	273	210	210	252
COM		922		

(1) AP-42 Emission Factors, Table 1.3.1

The applicant plans to fire No. 6 oil having a sulfur content of 1.0 percent instead of the 0.8 percent maximum presently allowed. The increase in sulfur dioxide emissions, as a result of burning the higher sulfur fuel, exceeds the significant emission rate of 40 tons per year and requires a BACT determination (17-2.500(5) (c)FAC) for the pollutant sulfur dioxide.

The applicant has submitted several applications that require a BACT determination. Three determinations have been made by combining similar sources as follows:

PART I - Sulfuric Acid Plants,
 PART II - Boiler Fuel Conversions
 PART III - DAP Dryer Fuel Conversion.

BACT Determination Requested by the Applicant:

Boilers, B, C, D, and E

Pollutant	Emission Limit
SO ₂ (oil)	1.1 lb/million BTU heat input (1% sulfur content)
SO ₂ (com)	0.9% sulfur content

Date of Receipt of a BACT application:

May 27, 1982

Date of Publication in the Florida Administrative Weekly:

June 11, 1982

Review Group Members:

The final determination was based upon comments received from the New Source Review Section and the Air Modeling Section.

BACT Determined by DER:

Auxiliary boiler E - Swift Creek Complex
Auxiliary boiler B, C, D - Suwannee River Complex

Sulfur dioxide emissions controlled by limiting the sulfur content of the No. 6 oil fired to a maximum of 1.0 percent and the COM fuel to 0.9 percent.

Compliance with the SO₂ emission limit will be based upon the Sulfur content of the fuel fired. Each shipment of fuel delivered to the facility will be sampled and the sulfur content determined and recorded. A certified analysis from the applicants fuel supplier may be substituted for on-site analysis. Applicable test methods by the American Society for Testing Material (A.S.T.M.) will be used.

Justification of DER Determination:

The facility is within 50 kilometers of the Okefenokee National Wilderness area, a Class 1 area. Air modeling indicates that at the conditions determined as BACT, the impact of sulfur dioxide emissions from the facility will be just less than the maximum allowable increase for a Class 1 area.

Details of the Analysis May Be Obtained by Contacting:

Edward Palagyi, BACT Coordinator
Department of Environmental Regulation
Bureau of Air Quality Management
2600 Blair Stone Road
Tallahassee, Florida 32301

Recommended By:

for *Steve Smallwood*
Steve Smallwood, Chief BAQM

Date: 11/7/82

Approved:

Victoria J. Tschinkel, Secretary

Date: _____

BEST AVAILABLE CONTROL TECHNOLOGY (BACT) DETERMINATION

PART III OF III

OCCIDENTAL CHEMICAL COMPANY

HAMILTON COUNTY

The applicant plans to increase the sulfur content of the fuel oil fired in the diammonium phosphate plant (DAP) dryer. The dryer is in the Suwannee River complex located near White Springs, Florida. The existing dryer is gas fired with No. 6 residual oil fired only during periods of gas curtailment. The sulfur content of the oil is to be increased to 1.5 percent from the presently permitted maximum of 0.8 percent.

At maximum dryer capacity No. 6 oil is fired at a rate of 246 gallons per hour. SO₂ emissions, at this rate of oil consumption (assume 80% SO₂ absorption), when firing 0.8% and 1.5% sulfur content oil is 6.3 and 11.8 pounds per hour respectively. The increase in SO₂ emissions would be 5.5 pounds per hour.

A Venturi scrubber in series with a packed tail-gas scrubber is used to reduce the air pollutants emitted in the dryer exhaust gases. Sulfur dioxide emissions are reduced by the control system, and, in addition, by reaction with the material being dried.

The applicant has submitted several applications that require a BACT determination. Three determinations have been made by combining similar sources as follows:

PART I - Sulfuric Acid Plants,
PART II - Boiler Fuel Conversions
PART III - DAP Dryer Fuel Conversion.

BACT Determination Requested by the Applicant:

Pollutant	Emission Limit
SO ₂	0.41 lb/ton P ₂ O ₅ input (fuel with 1.5% sulfur)

Date of Receipt of a BACT Application:

May 27, 1982

Date of Publication in the Florida Administrative Weekly:

June 11, 1982

Review Group Members:

The final determination was based upon comments received from the New Source Review Section and the Air Monitoring Section.

BACT Determined by DER:

Diammonium Phosphate Plant No. 2 product rotary dryer.
Suwannee River Chemical Complex

Sulfur dioxide emissions controlled by limiting the sulfur content of the No. 6 oil fired to a maximum of 1.5 percent, and SO₂ emissions to 0.20 lb. SO₂/ton DAP.

The applicant shall prepare a procedure to prevent the unloading of No. 6 oil containing 1.5% sulfur into the tank(s) which contain No. 6 oil having a lower sulfur content. A record will be kept of the amount of 1.5% oil received and the DAP dryer oil consumption rate. The records shall be made available to the department upon request.

Compliance with the SO₂ emission limit will be based upon the sulfur content of the fuel fired. Each shipment of fuel delivered to the facility will be sampled and the sulfur content determined and recorded. A certified analysis from the applicants fuel supplier may be substituted for on-site analysis. Applicable test methods by the American Society for Testing Material (A.S.T.M.) will be used.

Justification of DER Determination:

To reiterate per the BACT determination, Part II, the facility is within 50 kilometers of the Okefenokee National Wilderness area, a Class I area. Air modeling indicates that at the conditions determined as BACT, the impact of sulfur dioxide emissions from the facility will be just less than the maximum allowable increase for a Class I area.

The quantity of controlled SO₂ emissions from the dryer, when firing 1.5% sulfur content oil, is comparable to the amount of uncontrolled SO₂ emissions when firing 1.0% sulfur content oil. Oil is the stand-by fuel for this unit and would be fired only during periods of gas curtailment.

The use of the same grade fuel oil, but with different sulfur contents, will require, at the minimum, two fuel oil storage tanks. The applicant will have to set up a fuel oil handling procedure to prevent the transfer of the higher sulfur content oil to the wrong tank or other sources.

The department has determined, in this case, that the increase in the sulfur content of the oil fired (0.8% to 1.5%) is reasonable.

provided the anticipated 80% reduction in SO₂ emissions is documented.

Details of the Analysis May be Obtained by Contacting:

Edward Palagyi, BACT Coordinator
Department of Environmental Regulation
Bureau of Air Quality Management
2600 Blair Stone Road
Tallahassee, Florida 32301

Recommended By:

Ch. James

10x Steve Smallwood, Chief BAQM

Date: 11/2/82

Approved:

Victoria J. Tschinkel, Secretary

Date: _____

APPENDIX B

SPECIFIC CONDITIONS

FDER proposes a preliminary determination of approval with conditions for this project requested by Occidental Chemical Company in the permit applications submitted on June 8, 1982, (federal application) and May 21, 1982, (state application).

Special conditions listed in the State permits AC 24-56212, AC 24-56213, AC 24-56214, and AC 24-56215 are adopted as special conditions for the federal permit, PSD-FL-083, for these sources.

The attached General Conditions (federal) are also made a part of the proposed federal permit PSD-FL-083.