# STATE OF FLORIDA DEPARTMENT OF ENVIRONMENTAL PROTECTION NOTICE OF FINAL PERMIT.

In the Matter of an Application for Permit

Mr. John L. West Stone Container Corporation Post Office Box 26998 Jacksonville, Florida 32226-6998 DEP File No. 0310067-004-AC PSD-FL-252

Enclosed is the FINAL Permit Number PSD-FL-252 for increased steam production and heat input rate for the three existing boilers (Units 22, 23 and 26) at the Jacksonville Mill, Duval County. This permit is issued pursuant to Chapter 403, Florida Statutes and in accordance with Rule 62-212.400., F.A.C. - Prevention of Significant Deterioration (PSD).

Any party to this order (permit) has the right to seek judicial review of the permit pursuant to Section 120.68, F.S., by the filing of a Notice of Appeal pursuant to Rule 9.110, Florida Rules of Appellate Procedure, with the Clerk of the Department in the Legal Office; and by filing a copy of the Notice of Appeal accompanied by the applicable filing fees with the appropriate District Court of Appeal. The Notice of Appeal must be filed within 30 (thirty) days from the date this Notice is filed with the Clerk of the Department.

Executed in Tallahassee, Florida.

C.H. Fancy, P.E., Chief Bureau of Air Regulation

#### **CERTIFICATE OF SERVICE**

The undersigned duly designated deputy agency clerk hereby certifies that this NOTICE OF FINAL PERMIT (including the FINAL permit) was sent by certified mail (\*) and copies were mailed by U.S. Mail before the close of business on 3-9-00 to the person(s) listed:

John L. West, Stone Container Corp. \*

C. Kirts, DEP NED

J. Manning, RESD

B. Oven, DEP-OSC

D. Neely, EPA

j. Bunyak, NPS

D. Buff, Golder Associates

D. Roberts, Esq., HGSS

J. Antista, General Counsel, FG & FWFC

D. Russ, Esq., DCA

E.M. Barker, Esq., Slott & Barker

L.N. Curtin, Esq., Holland & Knight

G.K. Radlinski, Esq., City of Jacksonville

N.B. Barnard, Esq., St. Johns River WMD

R. Vandiver, General Counsel, PSC

Clerk Stamp

FILING AND ACKNOWLEDGMENT FILED, on this date, pursuant to §120.52, Florida Statutes, with the designated Department Clerk, receipt of which is hereby acknowledged.

(Clerk)

Date)

#### FINAL DETERMINATION

#### **Stone Container Corporation**

#### Permit No. 0310067-004-AC, PSD-FL-252

#### Jacksonville Mill

An Intent to Issue an air construction permit to Stone Container Corporation for an increase in the maximum steam production rate and heat input rate for each of the three package boilers at the Jacksonville Mill in Duval County, was distributed on January 11, 2000. The Notice of Intent was published in the Florida Times Union on January 22, 2000. Copies of the draft construction permit were available for public inspection at the Department offices in Jacksonville and Tallahassee.

No comments were submitted by the National Park Service, the U.S. Environmental Protection Agency or the public. The Department will remove the requirement in Specific Condition 11 of the permit of submitting the compliance test results to the Bureau of Air Regulation. The results will be submitted only to the Northeast District Office as well as RESD.

The final action of the Department is to issue the permit with the change noted above.

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## Department of Environmental Protection

Jeb Bush Governor Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

David B. Struhs Secretary

#### PERMITTEE:

Stone Container Corporation 9469 East Port Road Jacksonville, Florida 32229

Authorized Representative: Mr. John L. West, General Manager

**FID No.** 0310067

PSD No. PSD-FL-252

**SIC No.** 2621

**Project:** 3 Package Steam Boilers

Expires: January 31, 2001

#### PROJECT AND LOCATION:

Permit to increase the maximum steam production rate for each package boiler at the Stone Container Corporation Recycled Fiber Paper Mill in Jacksonville. Each of the three package boilers will be rated at 150,000 lb/hr steam at 650 psig and 750°F. The project is located at 9469 East Port Road, Jacksonville, Duval County. The UTM coordinates of this facility are Zone 17; 442.4 km E; 3365.4 km N.

#### STATEMENT OF BASIS:

This construction permit is issued under the provisions of Chapter 403 of the Florida Statutes (F.S.), and the Florida Administrative Code (F.A.C.) Chapters 62-4, 62-204, 62-210, 62-212, 62-296, and 62-297. The above named permittee is authorized to modify the facility in accordance with the conditions of this permit and as described in the application, approved drawings, plans, and other documents on file with the Department of Environmental Protection (Department).

#### Attached appendices are made a part of this permit:

Appendix BD

**BACT** Determination

Appendix GC

Construction Permit General Conditions

Howard L. Rhodes, Director

Division of Air Resources

Management

#### SECTION I. FACILITY INFORMATION

#### **FACILITY DESCRIPTION**

Stone Container Corporation (SCC) is a 100-percent recycled fiber paper mill facility located in Jacksonville, Duval County. Most of the steam required at SCC is provided by the adjacent U.S. Generating Company Cedar Bay Facility. The SCC facility includes three package boilers rated at 150,000 lb/hr steam at 650 psig and 750°F. These provide additional steam and serve as back-up when steam is not available from Cedar Bay.

#### REGULATORY CLASSIFICATION

The Stone Container facility is classified as a "Major or Title V Source" per Rule 62-210.200, F.A.C., because it has the potential to emit more than 100 tons per year of at least one regulated air pollutant.

This industry is included in the list of the 28 Major Facility Categories per Table 62-212.400-1, F.A.C. Because emissions are greater than 100 TPY for at least one regulated pollutant, the facility is a major facility with respect to Rule 62-212.400, Prevention of Significant Deterioration (PSD). Per Table 62-212.400-2, modifications at the facility resulting in emissions increases greater than the listed significance levels require review per the PSD rules and a determination of Best Available Control Technology (BACT) per Rule 62-212, F.A.C.

#### PERMIT SCHEDULE:

07-06-98: Date of Receipt of Application

12-07-99: Application complete

01-11-00: Issue Intent

01-22-00: Notice of Intent published in the Florida Times Union

#### **RELEVANT DOCUMENTS:**

The documents listed form the basis of the permit. They are specifically related to this permitting action. These documents are on file with the Department.

- Application received 07-06-98
- DEP Completeness Requests dated 08-04-98, 9-08-99, 09-10-99 and 09-22-99
- SCC's responses dated 08-12-99, 09-23-99, 10-07-99 and 12-07-99
- SCC's response to DEP's 3rd Completeness Request: 12-07-99
- Technical Evaluation and Preliminary Determination dated 01-11-00
- Best Available Control Technology determination (issued concurrently with permit)

#### SECTION II. EMISSION UNIT(S) GENERAL REQUIREMENTS

- 1. Regulating Agencies: All documents related to applications for permits to operate, reports, tests, minor modifications and notifications shall be submitted to the Department's Northeast District Office, 7825 Baymeadows Way, Jacksonville, Florida 32256-7590 and Regulatory & Environmental Services Department (RESD) in Jacksonville. All applications for permits to construct or modify an emissions unit(s) subject to the Prevention of Significant Deterioration or Nonattainment (NA) review requirements should be submitted to the Bureau of Air Regulation (BAR), Florida Department of Environmental Protection (FDEP), 2600 Blair Stone Road (MS 5505), Tallahassee, Florida 32399-2400 (phone number 850/488-0114).
- 2. <u>General Conditions</u>: The owner and operator is subject to and shall operate under the attached General Permit Conditions G.1 through G.15 listed in *Appendix GC* of this permit. General Permit Conditions are binding and enforceable pursuant to Chapter 403 of the Florida Statutes. [Rule 62-4.160, F.A.C.]
- 3. <u>Terminology</u>: The terms used in this permit have specific meanings as defined in the corresponding chapters of the Florida Administrative Code.
- 4. <u>Forms and Application Procedures</u>: The permittee shall use the applicable forms listed in Rule 62-210.900, F.A.C. and follow the application procedures in Chapter 62-4, F.A.C. [Rule 62-210.900, F.A.C.]
- 5. Expiration: This air construction permit shall expire on January 31, 2001 [Rule 62-210.300(1), F.A.C.]. The permittee may, for good cause, request that this construction permit be extended. Such a request shall be submitted to the Bureau of Air Regulation prior to 60 days before the expiration of the permit. However, the permittee shall promptly notify the Department's Northeast District Office and RESD of any delays in completion of the project which would affect the startup day by more than 90 days. [Rule 62-4.090, F.A.C]
- 6. <u>Application for Title V Permit</u>: An application for a Title V operating permit, pursuant to Chapter 62-213, F.A.C., must be submitted to the Department's Northeast District Office and RESD. [Chapter 62-213, F.A.C.]
- 7. New or Additional Conditions: Pursuant to Rule 62-4.080(1), F.A.C., for good cause shown and after notice and an administrative hearing, if requested, the Department may require the permittee to conform to new or additional conditions. The Department shall allow the permittee a reasonable time to conform to the new or additional conditions, and on application of the permittee, the Department may grant additional time. [Rule 62-4.080(1), F.A.C.]
- 8. <u>Annual Reports</u>: Pursuant to Rule 62-210.370(3), F.A.C., Annual Operating Reports, the permittee is required to submit annual reports on the actual operating rates and emissions from this facility. Annual operating reports shall be sent to the Department's Northeast District Office and RESD by March 1<sup>st</sup> of each year. [Rule 62-210.370(3), F.A.C.]

#### SECTION III. EMISSION UNIT(S) SPECIFIC CONDITIONS

The Specific Conditions listed in this section apply to the following emission units:

EMISSION UNIT NO.	System	Emission Unit Description
022	Process	Package Boiler No. 1
023	Process	Package Boiler No. 2
026	Process	Package Boiler No. 3

- 1. The construction and operation of these sources shall be in accordance with the capacities stated in the application dated June 1998. This permit shall replace PSD-FL-198(A).
- 2. The package boilers may each be operated continuously (8760 hrs/yr).
- 3. The maximum heat input rate to each boiler shall neither exceed 215 MMBtu/hr while firing natural gas nor 200 MMBtu/hr while firing No. 2 fuel oil.
- 4. In accordance with the terms of the Cedar Bay Cogeneration Project (CBCP) site certification, Stone Container Corporation (SCC) is limited to 640,000 lb/hr total steam consumption (380,000 lb/hr imported from CBCP and 260,000 lb/hr produced by SCC). When CBCP is not in operation or operating at reduced rates, SCC is permitted to produce up to 450,000 lb/hr steam and import up to 190,000 lb/hr from CBCP. This allows a maximum firing rate of 645 MMBtu/hr for all three package boilers when the CBCP facility is shutdown or operating at reduced rates.
- 5. The maximum allowable NO<sub>x</sub> emissions shall not exceed 0.2 lb/MMBtu, 34.94 lbs/hr and 153.1 tons/yr per boiler. The total NO<sub>x</sub> emissions from the three package boilers, in accordance with the terms of the CBCP site certification, shall not exceed 310 tons per year.
- 6. The three package boilers are permitted to fire both natural gas and No. 2 fuel oil, with the primary fuel being natural gas. The sulfur content of the No. 2 fuel oil shall not exceed 0.05 percent, by weight. Any delivery of No. 2 fuel oil shall be accompanied by a laboratory analysis quantifying the density and percent sulfur, by weight. Annual SO<sub>2</sub> emissions from No. 2 fuel oil firing, totaling all three boilers, shall not exceed 25 tons/year. In the event that the ceiling for SO<sub>2</sub> is expected to be exceeded due to unavailability of natural gas caused by factors beyond the control of SCC, SCC shall notify the Department that it anticipates exceeding the ceiling as provided herein; and, the emissions of SO<sub>2</sub> during the period of such curtailment shall not be counted against the yearly emissions ceiling of 25 tons unless administrative proceedings result in a finding that the exceedance was within SCC's control.

In no event shall the total annual emissions of SO<sub>2</sub> from the three steam boilers exceed 41 tons/year. The notice shall include a statement or reasons for the request and supporting documentation, and shall be published by SCC, without supporting documents, in a newspaper of general circulation in Jacksonville, Florida, as defined in Section 403.5115(2), F.S. The filing and publication of the notice no later than 7 days following the date of exceedance, shall preclude any finding of violation by the Department until final disposition of any administrative proceedings.

- 7. Visible emissions (VE) shall not exceed 5 percent (%) opacity during natural gas firing and 10% opacity during fuel oil firing.
- 8. In accordance with the requirements of 40 CFR 60.48b(b), a continuous emission monitoring system (CEMs) for nitrogen oxides shall be installed, operated, and maintained. Also, the natural gas, fuel oil and steam flows (both from the package boilers and from the CBCP facility) shall be metered and continuously recorded. The data shall be logged daily and maintained so that it can be provided to the Department upon request.
- 9. Before this construction permit expires, each package boiler shall be tested and monitored for compliance with the emission limits in Specific Conditions No. 3, 5, 6 and 7. For the duration of all tests the emission units shall be operating at permitted capacity. Permitted capacity is defined as 90-100 percent of the maximum operating rate allowed by the permit. If it is impracticable to test at permitted capacity, then the emission unit may be tested at less than permitted capacity (i.e., 90 percent of the maximum operating rate allowed by the permit); in this case, subsequent emission unit operation is limited to 110 percent of the test load until a new test is conducted. Once the emission unit is so limited, then operation at higher capacities is allowed for no more than 15 consecutive days for the purposes of additional compliance testing to regain the permitted capacity in the permit.
- 10. Compliance tests for NO<sub>x</sub> shall be conducted in accordance with 40 CFR 60.46b(e)(4). Compliance with SO<sub>2</sub> limits shall be in accordance with 40 CFR 60.49b(r), and a stoichiometric quantification for SO<sub>2</sub> emissions shall be utilized using the actual density and sulfur weight percent and the quantity of fuel oil fired monthly. Compliance with visible emission limits shall be demonstrated initially and annually in accordance with EPA Method 9.
- 11. The Department's Northeast District office and the RESD (City of Jacksonville's Regulatory and Environmental Services Department) office shall be notified at least 15 days prior to the compliance tests. Compliance test results shall be submitted to the Department's Northeast District and the RESD office within 45 days after completion of the tests. Sampling facilities, methods and reporting shall be in accordance with 40 CFR 60.49b, Chapter 62-297 and 40 CFR 60, Appendix A.
- 12. The permittee, for good cause, may request that this construction permit be extended. Such a request shall be submitted to the Department's Bureau of Air Regulation prior to 60 days before the expiration of the permit. (Rule 62-4.090, F.A.C.)

13. Pursuant to 40 CFR 60.49b(r), quarterly reports shall be submitted to the RESD office (i.e., Administrator) certifying that only very low sulfur oil (i.e., ≤0.05% sulfur, by weight) meeting this definition was combusted in the affected facility during the preceding quarter. The firing of any fuel oil and its associated SO₂ emissions shall be quantified on a monthly and per boiler basis and submitted to the RESD office by the end of the month following the end of each quarter. The quarters are defined as January-March, April-June, July-September and October-December; also, and per boiler, the final quarterly report shall include the total amount of the fuel oil fired and the quantified associated SO₂ emissions for the year.

#### Stone Container Corporation Recycled Fiber Paper Mill/ 3 Package Boilers PSD-FL-252 / 0310067-004-AC Jacksonville, Duval County

Stone Container Corporation (SCC) has applied to increase the maximum steam rate and heat input rate to the three package boilers. The boilers are operated to support the paper mill operations. The boilers are fired with natural gas or No. 2 fuel oil with a maximum sulfur content of 0.05 percent by weight. SCC is currently requesting an increase in the maximum steam production rate for each boiler from 125,000 lb/hr to 150,000 lb/hr steam. The Cedar Bay cogeneration facility that is located adjacent to the existing SCC facility provides part of the steam required for the recycle fiber facility. The recycle fiber facility requires additional steam beyond that provided by the Cedar Bay facility. SCC desires more flexibility in steam production in the case of a shutdown or curtailment by Cedar Bay. According to the terms of the Cedar Bay Site Certification proceedings, SCC is to be limited to a total steam consumption of 640,000 lb/hr, which includes 380,000 lb/hr, imported from the Cedar Bay facility. This leaves 260,000 lb/hr to be produced by the three package boilers under normal operating conditions. During periods when Cedar Bay facility is shut down or operating at reduced rates, SCC will be allowed to produce up to 450,000 lb/hr steam from the three package boilers and import up to 190,000 lb/hr steam from the Cedar Bay facility. The total steam consumption cap of 640,000 lb/hr for SCC will still be in place.

The project is subject to Prevention of Significant Deterioration (PSD) review for NO<sub>x</sub> in accordance with Rule 62-212.400, Florida Administrative Code (F.A.C.). A Best Available Control Technology (BACT) determination is part of the review required by Rules 62-212.400 and 62-296, F.A.C. Air pollution control equipment will consist of Low-NO<sub>x</sub> burners and flue gas recirculation to minimize NO<sub>x</sub> emissions from the 3 Package Boilers.

#### **PROCESS EMISSIONS**

The applicant proposes the following emissions:

POLLUTANT	EXISTING EMISSIONS (TPY)	PROPOSED EMISSIONS (TPY)	NET CHANGE IN EMISSIONS (TPY)	PSD REVIEW APPLIES?
PM	0.63	20.9	20.3	No
PM <sub>10</sub>	0.63	15.5	14.9	No
SO <sub>2</sub>	0.08	39.8	39.7	No
NO <sub>x</sub>	6.28	310	303.7	Yes

Stone Container Corporation 3 Package Boilers

DEP File No. 0310067-004-AC

PSD-FL-252

POLLUTANT	EXISTING EMISSIONS (TPY)	PROPOSED EMISSIONS (TPY)	NET CHANGE IN EMISSIONS (TPY)	PSD REVIEW APPLIES?
СО	2.62	58.4	55.8	No
VOC	0.18	3.88	3.70	No
Pb	3.40E-05	0.0072	0.0072	No -
Hg	1.88E-08	0.0022	0.0022	No
F	0.0	0.024	0.024	No
SAM	0.0	0.66	0.66	No

#### DATE OF RECEIPT OF COMPLETE BACT APPLICATION:

December 7, 1999

#### **BACT DETERMINATION PROCEDURE:**

In accordance with Chapter 62-212.400, F.A.C., this BACT determination is based on the maximum degree of reduction of each pollutant emitted which the Department of Environmental Protection (Department), on a case-by-case basis, taking into account energy, environmental and economic impacts, and other costs, determines is achievable through application of production processes and available methods, systems, and techniques. In addition, the regulations state that, in making the BACT determination, the Department shall give consideration to:

- Any Environmental Protection Agency determination of BACT pursuant to Section 169, and any emission limitation contained in 40 CFR Part 60 - Standards of Performance for New Stationary Sources or 40 CFR Part 61 - National Emission Standards for Hazardous Air Pollutants.
- All scientific, engineering, and technical material and other information available to the Department.
- The emission limiting standards or BACT determination of any other state.
- The social and economic impact of the application of such technology.

The EPA currently stresses that BACT should be determined using the "top-down" approach. The first step in this approach is to determine, for the emission unit in question, the most stringent control available for a similar or identical emission unit or emission unit category. If it is shown

that this level of control is technically or economically infeasible for the emission unit in question, then the next most stringent level of control is determined and similarly evaluated. This process continues until the BACT level under consideration cannot be eliminated by any substantial or unique technical, environmental, or economic objections.

#### **BACT EMISSION LIMITS PROPOSED BY APPLICANT:**

POLLUTANT	EMISSION LIMIT	CONTROL TECHNOLOGY
$NO_x$	0.2 lb/MMBtu, 34.94 lb/hr and 153.1 TPY	Low-NOx burners and FGR

#### **BACT ANALYSIS**

#### NITROGEN OXIDES (NO<sub>x</sub>)

Oxides of nitrogen ( $NO_x$ ) are generated during fuel combustion by oxidation of chemically bound nitrogen in the fuel (fuel  $NO_x$ ) and by thermal fixation of nitrogen in the combustion air (thermal  $NO_x$ ). As flame temperature increases, the amount of thermally generated  $NO_x$  increases. Fuel type affects the quantity and type of  $NO_x$  generated. Generally, natural gas is low in nitrogen. However it causes higher flame temperatures and generates more thermal  $NO_x$  than oil or coal, which have higher fuel nitrogen content, but exhibit lower flame temperatures.

NO<sub>x</sub> emissions represent a significant portion of the total emissions generated by this project, and must be minimized using BACT. A review of EPA BACT/LAER Clearinghouse (BACT Clearinghouse) information indicates that no boilers in the size range of the SCC boilers (i.e., 100-300 MMBtu/hr) which fire primarily natural gas have been required to install Selective Catalytic Reduction (SCR) or Selective Non-Catalytic Reduction (SNCR) as BACT. All have employed low-NO<sub>x</sub> burners and flue gas recirculation (FGR), which the SCC boilers employ.

The applicant has proposed combustion controls equipped on the three package boilers which includes FGR and low  $NO_x$  burners. The combination of FGR and low  $NO_x$  burners results in less  $NO_x$  formation. Low  $NO_x$  burners reduce  $NO_x$  by conducting the combustion process in stages. Staging partially delays the combustion process, resulting in a cooler flame which suppresses thermal  $NO_x$  formation.  $NO_x$  reductions of 40 to 85 percent (relative to uncontrolled emission levels) have been observed with low  $NO_x$  burners when combined with flue gas recirculation.

In a FGR system, a portion of the flue gas is recycled from the stack to the burner windbox. Upon entering the windbox, the cooler gas is mixed with combustion air prior to being fed to the burner. The FGR system reduces NO<sub>x</sub> emissions by two mechanisms. In the first mechanism, the recycled flue gas is made up of combustion products which acts as inerts during combustion of the fuel/air mixture. This additional mass is heated in the combustion zone, thereby lowering the peak flame temperature and reducing the amount of NO<sub>x</sub> formed. Second, to a lesser extent, FGR also reduces NO<sub>x</sub> formation by lowering the oxygen concentration in the primary flame zone. **This** 

combination of NO, controls and good combustion practices should provide effective emissions control.

#### BACT DETERMINATION BY THE DEPARTMENT:

Based on the information provided by the applicant and the information searches conducted by the Department, lower emissions limits can be obtained employing the top-down BACT approach for NO.

#### NO, DETERMINATION

The top-down BACT approach for natural gas/fuel oil boilers listed in order from most stringent control to least:

- 1. Selective Catalytic Reduction (SCR)
- 2. Selective Noncatalytic Reduction (SNCR)
- 3. Good combustion design/practices

The following table summarizes the feasibility of using these control technologies with the Package Boilers as designed for installation in SCC Recycle Fiber Paper Mill.

Control Technology	Emission Reduction (%)	Technically Feasible	Cost per ton	Adverse Environ. Impacts
SCR with ammonia	80-90	Yes	\$4,600	Yes
SNCR	40-70	Yes	\$8,000	No
Low NO <sub>x</sub> Burners with Flue Gas Recirculation	20-50	Yes	N/A	No

Assuming maximum boiler operation, the cost per ton for SCR is about \$4,600/ton. Using a still very conservative annual capacity factor of 50 percent, the cost effectiveness increases to more than \$7,300/ton. This economic impact is very high considering that normally SCC's boilers will not operate or will operate at very reduced rates, since Cedar Bay will provide the majority of the steam to SCC. For NO<sub>x</sub> emissions, the Department accepts the applicants proposed use of low NO<sub>x</sub> burners with flue gas recirculation as BACT for this project.

The BACT emission level established by the Department is as follows:

POLLUTANT	EMISSION LIMIT
Nitrogen Oxides (NO <sub>x</sub> )	0.2 lb/mmBtu; 34.94 lb/hr and 153.1 TPY. Total NO <sub>x</sub> emissions from 3 package boilers is limited to 310 TPY.

#### **COMPLIANCE**

Each package boiler shall be tested and monitored for compliance with the  $NO_x$  emission limits in accordance with 40 CFR 60.46b(e)(4).

#### DETAILS OF THE ANALYSIS MAY BE OBTAINED BY CONTACTING:

Syed Arif, P.E., Permit Engineer

Department of Environmental Protection

Bureau of Air Regulation - MS 5505

2600 Blair Stone Road

Tallahassee, Florida 32399-2400

Recommended By:

Approved By:

C. H. Fancy, P.E., Chief Bureau of Air Regulation

3/8/00

Date:

Howard L. Rhodes, Director

Division of Air Resources Management

Data

#### GENERAL PERMIT CONDITIONS [F.A.C. 62-4.160]

- G.1 The terms, conditions, requirements, limitations, and restrictions set forth in this permit are "Permit Conditions" and are binding and enforceable pursuant to Sections 403.161, 403.727, or 403.859 through 403.861, Florida Statutes. The permittee is placed on notice that the Department will review this permit periodically and may initiate enforcement action for any violation of these conditions.
- G.2 This permit is valid only for the specific processes and operations applied for and indicated in the approved drawings or exhibits. Any unauthorized deviation from the approved drawings or exhibits, specifications, or conditions of this permit may constitute grounds for revocation and enforcement action by the Department.
- G.3 As provided in Subsections 403.087(6) and 403.722(5), Florida Statutes, the issuance of this permit does not convey and vested rights or any exclusive privileges. Neither does it authorize any injury to public or private property or any invasion of personal rights, nor any infringement of federal, state or local laws or regulations. This permit is not a waiver or approval of any other Department permit that may be required for other aspects of the total project which are not addressed in the permit.
- G.4 This permit conveys no title to land or water, does not constitute State recognition or acknowledgment of title, and does not constitute authority for the use of submerged lands unless herein provided and the necessary title or leasehold interests have been obtained from the State. Only the Trustees of the Internal Improvement Trust Fund may express State opinion as to title.
- G.5 This permit does not relieve the permittee from liability for harm or injury to human health or welfare, animal, or plant life, or property caused by the construction or operation of this permitted source, or from penalties therefore; nor does it allow the permittee to cause pollution in contravention of Florida Statutes and Department rules, unless specifically authorized by an order from the Department.
- G.6 The permittee shall properly operate and maintain the facility and systems of treatment and control (and related appurtenances) that are installed or used by the permittee to achieve compliance with the conditions of this permit, as required by Department rules. This provision includes the operation of backup or auxiliary facilities or similar systems when necessary to achieve compliance with the conditions of the permit and when required by Department rules.
- G.7 The permittee, by accepting this permit, specifically agrees to allow authorized Department personnel, upon presentation of credentials or other documents as may be required by law and at a reasonable time, access to the premises, where the permitted activity is located or conducted to:
  - (a) Have access to and copy and records that must be kept under the conditions of the permit;
  - (b) Inspect the facility, equipment, practices, or operations regulated or required under this permit, and,
  - (c) Sample or monitor any substances or parameters at any location reasonably necessary to assure compliance with this permit or Department rules.

Reasonable time may depend on the nature of the concern being investigated.

- G.8 If, for any reason, the permittee does not comply with or will be unable to comply with any condition or limitation specified in this permit, the permittee shall immediately provide the Department with the following information:
  - (a) A description of and cause of non-compliance; and
  - (b) The period of noncompliance, including dates and times; or, if not corrected, the anticipated time the non-compliance is expected to continue, and steps being taken to reduce, eliminate, and prevent recurrence of the non-compliance.

The permittee shall be responsible for any and all damages which may result and may be subject to enforcement action by the Department for penalties or for revocation of this permit.

- In accepting this permit, the permittee understands and agrees that all records, notes, monitoring data and other information relating to the construction or operation of this permitted source which are submitted to the Department may be used by the Department as evidence in any enforcement case involving the permitted source arising under the Florida Statutes or Department rules, except where such use is prescribed by Sections 403.73 and 403.111, Florida Statutes. Such evidence shall only be used to the extent it is consistent with the Florida Rules of Civil Procedure and appropriate evidentiary rules.
- G.10 The permittee agrees to comply with changes in Department rules and Florida Statutes after a reasonable time for compliance, provided, however, the permittee does not waive any other rights granted by Florida Statutes or Department rules.
- G.11 This permit is transferable only upon Department approval in accordance with Florida Administrative Code Rules 62-4.120 and 62-730.300, F.A.C., as applicable. The permittee shall be liable for any non-compliance of the permitted activity until the transfer is approved by the Department.
- G.12 This permit or a copy thereof shall be kept at the work site of the permitted activity.
- G.13 This permit also constitutes:
  - (a) Determination of Best Available Control Technology (X)
  - (b) Determination of Prevention of Significant Deterioration (X); and
  - (c) Compliance with New Source Performance Standards (X).
- G.14 The permittee shall comply with the following:
  - (a) Upon request, the permittee shall furnish all records and plans required under Department rules. During enforcement actions, the retention period for all records will be extended automatically unless otherwise stipulated by the Department.
  - (b) The permittee shall hold at the facility or other location designated by this permit records of all monitoring information (including all calibration and maintenance records and all original strip chart recordings for continuous monitoring instrumentation) required by the permit, copies of all reports required by this permit, and records of all data used to complete the application or this permit. These materials shall be retained at least three years from the date of the sample, measurement, report, or application unless otherwise specified by Department rule.
  - (c) Records of monitoring information shall include:
    - 1. The date, exact place, and time of sampling or measurements;
    - 2. The person responsible for performing the sampling or measurements;
    - 3. The dates analyses were performed;
    - 4. The person responsible for performing the analyses;
    - 5. The analytical techniques or methods used; and
    - 6. The results of such analyses.
- G.15 When requested by the Department, the permittee shall within a reasonable time furnish any information required by law which is needed to determine compliance with the permit. If the permittee becomes aware that relevant facts were not submitted or were incorrect in the permit application or in any report to the Department, such facts or information shall be corrected promptly.

#### Memorandum

### Florida Department of **Environmental Protection**

TO:

Howard L. Rhodes

THRU:

FROM

Syed Arif

DATE:

February 28, 2000

SUBJECT: Stone Container Corporation, 0310067-004-AC,

PSD-FL-252

Attached for your approval and signature is a construction permit to increase the maximum steam production rate and heat input rate for each of the three existing package boilers at Stone Container in Jacksonville, Duval County, Florida.

Stone Container used to be a Kraft Mill but now relies solely on recycled fiber. Several years ago Stone Container shut down its regular boilers allowing Cedar Bay Cogen to build a facility next door. Stone is now basically a "steam host" for Cedar Bay.

To provide for occasional interruption of steam from Cedar Bay, Stone Container installed three packaged boilers that operate almost exclusively on natural gas. The steam production rate from each was limited to levels well below capacity. Stone Container wants to increase the maximum production rate from 125,000 lb/hr to 150,000 lb/hr while maintaining their current permitted emission levels for NO, and SO2.

Because the boilers are restricted to back-up service, historical NO<sub>x</sub> emissions have only been about 6 tons per year of NO<sub>X</sub>. However potential emissions are 310 TPY so that PSD was triggered on a past actual to future potential emission comparison.

A Technical Evaluation and Preliminary Determination was issued, and the facility was required to do a public notice. A Best Available Control Technology determination was required for NO<sub>x</sub> pursuant to Rule 62-212.400, F.A.C. NO<sub>x</sub> emissions will be controlled through low-NO<sub>x</sub> burners and flue gas recirculation. If the units were new and operated continuously, we might have specified selective catalytic reduction.

Many parties were involved during the certification of Cedar Bay and the conversion of Stone Container to a recycling facility. They were all copied on the Intent and none provided comments.

The project modification provides reasonable assurance that all the requirements of the permit and BACT determination will be complied with. I recommend your approval and signature.

SA/a

Attachments

### RECEIVED

THE FLORIDA TIMES-UNION

FEB 0 4 2000

Jacksonville, Fl

Affidavit of Publication BUREAU OF AIR REGULATION

Florida Times-Union

SMURFIT-STONE CONTAINER CORP RECEIVED PO BOX 26998

JACKSONVILLE FL 32226

REFERENCE: 0527634

R01687

Public Notice Of Int

State of Florida County of Duval

Before the undersigned authority personally appeared Steven L. Smith who on cath says he is a Legal Advertising Representative of The Florida Times-Union, a daily newspaper published in Jacksonville in Duval County, Florida; that the attached copy of advertisement is a legal ad published in The Florida Times-Union. Affiant further says that The Florida Times-Union is a newspaper published in Jacksonville, in Duval County, Florida, and that the newspaper has heretofore been continuously published in Duval County, Florida each day, has been entered as second class mail matter at the post office in Jacksonville, in Duval County, Florida for a period of one year preceeding the first publication of the attached copy of advertisement; | and affiant further says that he/she has neither paid nor promised any person, firm or corporation any discount, rebate, commission, or refund for the purpose of securing this advertisement for publication in said newspaper.

PUBLISHED ON: 01/22

01/22/00

PUBLIC NOTICE OF INTENT TO ISSUE PSD PERMIT
STATE OF FLORIDA
DEPARTMENT OF ENVIRONMENTAL PROTECTION
DEP File No. 0310067-004-AC (PSD-FL-252)
Duval County, Florida

The Department of Environmental Protection (Department) gives notice of its intent to, issue a permit under the requirements for the Prevention of Significant Deterioration of Air Quality-(PSD permit) to Stone Container Corporation. The permit will allow an increase in the maximum steam production rate and heat input rate for each of the three existing package boilers at its Jacksonville Mill in Duval County, Florida. The three package boilers are operated to support the recycled paper mill operations. Each of the three package boilers will increase the steam production rate from 125,000 lb/hr ta 150,000 lb/hr, but will maintain the current permitted emission levels for nitrogen oxides (NO.) and sulfur dioxide (SO<sub>2</sub>).

Maximum heat input rate to each boiler will be 215 MMBtu/hr when firing natural gas, and 200 MMBtu/hr when firing No. 2 fuel oil. A Best Available Control

Technology (BACT) determination was required for  $\rm NO_X$  pursuant to Rule 62-212.400, F.A.C.

The applicant's name and address are Stone Container Corporation, Post office Box 26998, Jocksonville, Florida 32226-6998. The Jacksonville Mill is located at 9469 East Port Road, Jacksonville, Duval County, Florida.

NO<sub>X</sub> emissions from the package boilers will be controlled through low-NO<sub>x</sub> burners and Flue Gas Recirculation.

The net emissions increase due to the increased steam production for PSD applicability purposes is summarized below (in tons per year).

Net Emissions Increase 304 PSD Significant Emission Rate <u>Pollutant</u>

An air quality impact analysis was conducted for NO<sub>X</sub>. Emissions from the facility will not significantly contribute to or cause a violation of any state or federal

ambient air quality standards.

The Department will accept written comments and requests for a public The Department will accept written comments and requests for a public meeting concerning the proposed permit issuance action for a period of 30 (thirty) days from the date of publication of this "Public Notice of Intent to Issue PSD permit." Written comments and requests for a public meeting should be provided to the Department's Bureau of Air Regulation at 2600 Blair Stone Road, Mail Station #5505, Tallahassee, Florida 32399-2400. Any written comments filed shall be made available for public inspection.

The Department will issue the permit with the attached conditions unless a timely existing for an administrative hopping is filed ourselant to Sections 120,549 and

The Department will issue the permit with the attached conditions unless a timely petition for an administrative hearing is filed pursuant to Sections 120.569 and 120.57 of the Florida Statutes. The petition must contoin the information set forth below and must be filed (received) in the Office of General Counsel of the Department, 3900 Commonwealth Boulevard, Mail Station #35, Tallahassee, Florida 32399-3000. Petitions filed by the permit applicant or any of the parties listed below must be filed within fourteen (14) days of receipt of this notice of intent. Petitions filed by any persons other than those entitled to written notice under Section 120.60(3) of the Florida Statutes must be filed within fourteen days of publication of the public notice or within fourteen (14) days of receipt of this notice of intent, whichever occurs first. Under Section 120.60(3), however, any person who asked the Department for notice of agency action may file a petition within fourteen (14) days of receipt of that notice, regardless of the date of publication. A petitioner shall mail Department for notice of agency action may file a petition within tourteen (14) days of receipt of that notice, regardless of the date of publication. A petitioner shall mail a copy of the petition to the applicant at the address indicated above of the time of filing. The failure of any person to file a petition within the appropriate time period shall constitute a waiver of that person's right to request an administrative determination (hearing) under Sections 120.569 and 120.57, Florida Statutes, or to intervene in this proceeding and participate as a party to it. Any subsequent intervention will be only at the approval of the presiding officer upon the filing of a motion in compliance with Rule 28-106.205 of the Florida Administrative Code.

A petition that disputes the material facts on which the Department's action is based must contain the following information: (a) The name and address of each ogency affected and each agency's file or identification number, if known; (b) The name, address and telephone number of the petitioner, the name, address, and telephone number of the petitioner's representative, if any which shall be the telephone number of the petitioner's representative, if any which shall be the address for service purposes during the course of the proceeding; and explanation of how the petitioner's substantial interests will be affected by the agency determination; (c) A statement of how and when petitioner received notice of the agency action or proposed action; (d) A statement of oll disputed issues of material facts. If there are none, the petition must so indicote; (e) A concise statement of the ultimate facts alleged, as well as the rules and statutes which entitle the petitioner to relief; and (f) a demand for relief.

A petition that does not dispute the material facts upon which the Department's action is based shall state that no such facts are in dispute and otherwise shall.

oction is based shall state that no such facts are in dispute and otherwise shall contain the some information as set forth obove, os required by Rule 28-106.301 of the Florido Administrative Code.

Because the administrative hearing process is designed to formulate final ogency action, the filing of a petition means that the Department's final action may be different from the petition taken by it in this notice. Persons whose substantial interests will be affected by any such final decision of the Department on the application have the right to petition to become a party to the proceeding, in accordance with the requirements set forth obove.

A complete project file is available for public inspection during normal business hours, 8:00 a.m. to 5:00 p.m., Monday through Friday, except legal holidays, at: Department of Environmental Protection Department of Environmental Protection Northeast District Office
7825 Baymeadows Way, Suite 200B
Jocksonville, Florida 32256-7590
Telephone: 904/448-4300

Bureau of Air Regulation 111 South Magnolia Drive, Suite 4 Tallahassee, Fiorida 32301 Telephone: 850/488-1344

Fax: 850/922-6979 Fax: 904/448-4366 Regulatory & Environmental Services Department (RESD) Suite 225, 117 W. Duval Street Fax: 904/448-4366

Jacksonville, Florida 32202 Telephone: 904/630-3484 Fax: 904/630-3638

The complete project file includes the Draft Permit, the application and the information submitted by the responsible official, exclusive of confidential records under Section 403.111, Florida Statutes. Interested persons may contact the New Resource Review Section at 111 South Mognolia Drive, Suite 4, Tallahossee, Florida 32301, or call 850/488-0114, for additional information.

Name: Staven L. Smith

Title: Legal Advertising Representative

In testimony whereof, I have hereunto set my hand and affixed my official

seal, the day and year aforesaid.

Lmud Culch

OFFICIAL NOTARY SEAL JANICE I WEEKS COMMISSION NUMBER CC855805 MY COMMISSION EXPIRES

AUG 15.2003



### **Best Available Copy**

### SMURFIT-STONE CONTAINER CORPORATION

### **FACSIMILE**

NO. OF PAGES 🚨 🔃

TO: 7DEP Bureau of Air Regulation
FROM: W. Joe Eskridge

LOCATION: TallahassEE, FL

LOCATION: SSCC JA

#### MESSAGE:

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From the deak of: W. Joe Eskrida Environmental Engineer Smurfit-Stone Container Corporation Phone: [904] 714-3225 Fax: [904] 714-3278

THE PLORIDA TIMES-UNION Jacksonville, Fl Affigavit of Publication

Florida Times-Union

SMURFIT-STONE CONTAINER CORP RECEIVEN PC BOX 26998 JACKSONVILLE FL 32226

ESSEPENCE: 0527634

R31€37

Public Notice Of Int

State of Florida County of Daval

Before the undersigned authority personally appeared Steven L. Smith who on oath says he is a Legal Advertising Representative of The Florida Times-Union, a daily newspaper published in Jacksonville in Duval County, Florida; that the attached copy of advertisement is a legal ad published in The Florida Times-Union. Affiant further says that The Florida Times-Union is a newspaper published in Jacksonville, in Duval County, Florida, and that the newspaper has herecofore been continuously published in Duval County, Florida each day, has been entered as second class mail matter at the post office in Jacksonville, in Duyal County, Florida for a period of one year proceeding the first publication of the attached copy of advertisement; and affiant further mays that he/she has neither paid nor promised any person, firm or corporation any discount, rebate, commission, or refund for the purpose of securing this advertisement for publication in said newspaper.

17. PUBLISHED ON: 01/22,

67 m

aya shi ul ; .t.\*.

FILED ON:

Name: Steven L. Smith

٠,٠.

Title: Legal Advertising Representative

In testimony whereof, I have hereunto set my hand and affixed my official

seal, the day and year aforesaid.

Knaud Week VOTARY.

CHICAL BUTART SEA COMMISSION NUMBER CCRA6805 LINESKON EXPIRES AUG. 15,2003

SMURFIT STONE 2NDFLR

DEP File No. 031067-004-AC (PSD-FL-252)

DEP File No. 031067-004-AC (PSD-FL-252)

Devail County, Florida

The Department of Environmental Protection (Department) gives notice at its intent to asse a permit under the requirements for the Prevention of Significant Deterioration at its dustitive (PSD-wermit) to Stone Container Corporation. The permit will allow an increase in the maximum steam production rate and heat input rate for each of the innee existing eackage boilers at its Jacksonville Mill in Duvel County, Florida. The three pockage boilers at its Jacksonville Mill in Duvel County, Florida. The three pockage boilers are operated to support the recycled paper mill operations. Each at the three pockage boilers will increase the steam production rate from 125,000 lbnr. to.150,000 lbnr. but will mointain the current permitted emission levels for nitrogen axides (No.) and sulfur disade (So.).

Maximum heat input rate to each boiler will be 215 MMBTu/nr when tiring notured acc, and 200 MMBTu/nr when firing No. 2 fuel oil. A Best Available Control Technology (BACT) defermination was required for Nox pursuant to Rule 62-112.400, F.A.C.

The applicant's nome and address are stone Container Corporation, Post office Box 26998, Jacksonville, Florida 32226-6998. The Jacksonville Mill is located at 9469 East Port Road, Jacksonville, Duval County, Florida.

Nox emissions from the package boilers will be confroiled through law-Nox burners and Flue Gas Rectroviation.

The net emissions increase due to the increased steam production for SD applicability purposes is summarized below (in tone per year).

Pollutant Net Emissions Increase

PSD Significant Emission Role\*\*

SMURFIT STONE 2NDFLR

Pollutont Net Emissions Increase PSD Significant Emission Role\*\*

An air quality impact analysis was conducted for NO<sub>X</sub>. Emissions from the tacility will not significantly contribute to or cause a violation of any state or federal

An air quality impact analysis was conducted for NO<sub>X</sub>. Emissions from the tacility will not significantly contribute to are cause a violation of any state or federal ambient air quality standards.

The Department will accept written comments and requests for a public meeting concerning the proposed permit issuance action for a period of 30 (thirty) days from the date of publication of this "Public Notice of Intent to Issue PSD permit." Written comments and requests for a public meeting should be provided to the Department's Bureau of Air Regulation of 2600 Blair State Road. Mall Station #5505, Tallahassee, Flarida 32399-2400. Any written comments fitted shall be made evallable for public inspection.

The Department will issue the permit with the attached conditions unless a timely petition for an administrative hearing is fitted pursuant to Sections 120.569 and 120.57 of the Flarida Statutes. The petition must contain the information set forth below and must be fitted (received) in the Office of General Counsel at the Department, 3900 Commonwealth Boutevard, Mall Station #35, Tallahassee, Flarida 2239-3000, Petitions filled by the permit applicant or any of the parties listed below must be tiled within fourteen (14) days of receipt of this notice under Section 120.60(3) of the Florida Statutes must be filled within fourteen agree of intent, Petitions filled by any persons other than those entitled to written notice under Section 120.60(3), however, any person who asked the Department for notice of agency action may file a petition within tourteen (14) days of receipt of this notice of intent, whichever occurs first. Under Section 120.60(3), however, any person who asked the Department for notice of agency action may file a petition within tourteen (14) days of receipt of that notice, regardless of the date of publication. A petitioner shall mail a capy of the petitioner of that person's right to request an administrative deal constitute a waiver of that person's right to request an administrative deal constitu

how the petitioner's substantial interests will be affected by the agency determination; (c) A statement of how and when petitioner received notice of the agency action or proposed action; (d) A statement of all disputed issues of material facts. If there are none, the petition must so indicate; (e) A concise statement of the utilimate facts alleged, as well as the rules and statutes which entitle the petitioner to relief; and (f) a demand for relief.

A petition that does not dispute the material facts upon which the Department's action is based shall state that no such facts are in dispute and otherwise shall contain the same information as set forth above, as required by Rule 28-106.301 of

the Florida Administrative Code.

Because the administrative hearing process is designed to formulate final agency action, the filing of a petition means that the Department's final action may be different from the petition taken by it in this notice. Persons whose substantial interests will be affected by any such final decision of the Department on the application have the right to petition to become a party to the proceeding, in accordance with the requirements set forth above.

A complete project file is available for public inspection during normal business indurs, 8:00 a.m. to 5:00 p.m., Manday through Friday, except legal holidays, at:

Department of Environmental Protection
Bureau of Air Regulation
Post Magnalia Drive, Suite 4
Tallahassee, Florida 32301
Telephone: 850/488-1344
Fax: 850/922-6979
Department of Environmental Protection
Northeast District Office
7825 Baymeadows Way, Suite 200B
Jocksonville, Florida 32256-7590
Telephone: 904/488-4300
Fax: 904/448-4300
Fax: 904/448-4300 avreau of Air Regulation 311 South Magnolla Drive, Suite 4 Tallahassee, Florida 32301 Telephone: 850/488-1344 Fax: 850/922-6979

Regulatory & Environmental Services Department (RESD) Suite 225, 117 W. Duval Street Jacksonville, Florida 32202
Telephone: 904/630-3484 and the state of t

Fax: 904/630-3638 Fax: 904/830-3038

The complete project file includes the Draft Permit, the application and the information submitted by the responsible official, exclusive of confidential records under Section 403.111, Florida Statutes. Inferested persons may contact the New Resource Review Section at 111 South Magnolia Drive, Sulte 4, Tallohassee, Florida 32301, or call 850/488-0114, for additional information.



# Department of Environmental Protection

Jeb Bush Governor Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

David B. Struhs Secretary

January 5, 2000

CERTIFIED MAIL - RETURN RECEIPT REQUESTED

Mr. John L. West, General Manager Stone Container Corporation Post Office Box 26998 Jacksonville, Florida 32226-6998

Re: DEP File No. 0310067-004-AC (PSD-FL-252)

Recycled Fiber Paper Mill

3 Package Boilers

Dear Mr. West:

Enclosed is one copy of the Draft Permit, Technical Evaluation and Preliminary Determination, for the referenced project in Duval County. The Department's Intent to Issue Permit and the "<u>PUBLIC NOTICE OF INTENT TO ISSUE</u>" are also included.

The "Public Notice of Intent to Issue Permit" must be published as soon as possible in a newspaper of general circulation in the area affected. Proof of publication, i.e., newspaper affidavit, must be provided to the Department's Bureau of Air Regulation within 7 (seven) days of publication. Failure to publish the notice and provide proof of publication within the allotted time may result in the denial of the permit.

Please submit any written comments you wish to have considered concerning the Department's proposed action to A. A. Linero, P.E., Administrator, New Source Review Section, at the above letterhead address. If you have any questions, please call Syed Arif at 850/921-9528.

Sincerely,

C. H. Fancy, P.E., Chief, Bureau of Air Regulation

CHF/sa

Enclosures

In the Matter of an Application for Permit by:

Mr. John L. West, General Manager Stone Container Corporation Post Office Box 26998 Jacksonville, FL 32226-6998 DEP File No. 0310067-004-ACDRAFT Permit No. PSD-FL-252 Recycled Fiber Paper Mill 3 Package Boilers Duval County

#### INTENT TO ISSUE PSD PERMIT

The Florida Department of Environmental Protection (Department) gives notice of its intent to issue a permit under the requirements for the Prevention of Significant Deterioration (PSD) of Air Quality (copy of Draft PSD Permit attached) for the proposed project, detailed in the application specified above and the attached Technical Evaluation and Preliminary Determination, for the reasons stated below.

The applicant, Stone Container Corporation, applied on July 6, 1998, to the Department for a PSD permit to increase maximum steam production rate for each of the three boilers at its existing Jacksonville Mill in Duval County, Florida.

The Department has permitting jurisdiction under the provisions of Chapter 403, Florida Statutes (F.S.), and Florida Administrative Code (F.A.C.) Chapters 62-4, 62-210, and 62-212. The above actions are not exempt from permitting procedures. The Department has determined that a PSD permit and a determination of Best Available Control Technology for the control of nitrogen oxide is required to conduct the work.

The Department intends to issue this PSD permit based on the belief that reasonable assurances have been provided to indicate that operation of these emission units will not adversely impact air quality, and the emissions units will comply with all appropriate provisions of Chapters 62-4, 62-204, 62-210, 62-212, 62-296, and 62-297, F.A.C.

Pursuant to Section 403.815, F.S., and Rule 62-110.106(7)(a)1., F.A.C., you (the applicant) are required to publish at your own expense the enclosed "Public Notice of Intent to Issue PSD Permit." The notice shall be published one time only in the legal advertisement section of a newspaper of general circulation in the area affected. For the purpose of these rules, "publication in a newspaper of general circulation in the area affected" means publication in a newspaper meeting the requirements of Sections 50.011 and 50.031, F.S., in the county where the activity is to take place. Where there is more than one newspaper of general circulation in the county, the newspaper used must be one of significant circulation in the area that may be affected by the permit. If you are uncertain that a newspaper meets these requirements, please contact the Department at the address or telephone number listed below.

The applicant shall provide proof of publication to the Department's Bureau of Air Regulation, 2600 Blair Stone Road, Mail Station #5505, Tallahassee, Florida 32399-2400 (Telephone: 850-488-0114; Fax 850/922-6979). The Department suggests that you publish the notice within thirty days of receipt of this letter. You must provide proof of publication within seven days of publication, pursuant to Rule 62-110.106(5), F.A.C. No permitting action for which published notice is required shall be granted until proof of publication of notice is made by furnishing a uniform affidavit in substantially the form prescribed in Section 50.051, F.S., to the office of the Department issuing the permit or other authorization. Failure to publish the notice and provide proof of publication may result in the denial of

DEP File No. 0310067-004-AC, PSD-FL-252 Page 2 of 3

the permit pursuant to Rules 62-110.106(9) & (11), F.A.C.

The Department will issue the final permit with the attached conditions unless a response received in accordance with the following procedures results in a different decision or significant change of terms or conditions.

The Department will accept written comments and requests for a public meeting concerning the proposed permit issuance action for a period of thirty (30) days from the date of publication of "Public Notice of Intent to Issue PSD permit." Written comments and requests for a public meeting should be provided to the Department's Bureau of Air Regulation at 2600 Blair Stone Road, Mail Station #5505, Tallahassee, FL 32399-2400. Any written comments filed shall be made available for public inspection.

The Department will issue the permit with the attached conditions unless a timely petition for an administrative hearing is filed pursuant to sections 120.569 and 120.57, F.S., before the deadline for filing a petition. The procedures for petitioning for a hearing are set forth below. Mediation is not available in this proceeding.

A person whose substantial interests are affected by the proposed permitting decision may petition for a administrative proceeding (hearing) under Sections 120.569 and 120.57, F.S. The petition must contain the information set forth below and must be filed (received) in the Office of General Counsel of the Department at 3900 Commonwealth Boulevard, Mail Station #35, Tallahassee, Florida, 32399-3000. Petitions filed by the permit applicant or any of the parties listed below must be filed within fourteen days of receipt of this notice of intent. Petitions filed by any persons other than those entitled to written notice under section 120.60(3) of the Florida Statutes must be filed within fourteen days of publication of the public notice or within fourteen days of receipt of this notice of intent, whichever occurs first. Under Section 120.60(3), F.S., however, any person who asked the Department for notice of agency action may file a petition within fourteen days of receipt of that notice, regardless of date of publication. A petitioner shall mail a copy of the petition to the applicant at the address indicated above at the time of filing. The failure of any person to file a petition within the appropriate time period shall constitute a waiver of that person's right to request an administrative determination (hearing) under Sections 120.569 and 120.57, F.S., or to intervene in this proceeding and participate as a party to it. Any subsequent intervention will be only at the approval of the presiding offer upon the filing of a motion in compliance with Rule 28-106.205 of the Florida Administrative Code (F.A.C.)

A petition that disputes the material facts on which the Department's action is based must contain the following information: (a) The name and address of each agency affected and each agency's file or identification number, if known; (b) The name, address, and telephone number of the petitioner, the name, address, and telephone number of the petitioner's representative, if any, which shall be the address for service purposes during the course of the proceeding; and an explanation of how the petitioner's substantial interests will be affected by the agency determination; (c) A statement of how and when petitioner received notice of the agency action or proposed action; (d) A statement of all disputed issues of material fact. If there are none, the petition must so indicate; (e) A concise statement of the ultimate facts alleged, as well as the rules and statutes which entitle the petitioner to relief; and (f) A demand for relief.

A petition that does not dispute the material facts upon which the Department's action is based shall state that no such facts are in dispute and otherwise shall contain the same information as set forth above, as required by Rule 28-106.302, F.A.C.

# DEP File No. 0310067-004-AC, PSD-FL-252 Page 3 of 3

Because the administrative hearing process is designed to formulate final agency action, the filing of a petition means that the Department's final action may be different from the position taken by it in this notice. Persons whose substantial interests will be affected by any such final decision of the Department on the application have the right to petition to become a party to the proceeding, in accordance with the requirements set forth above.

Executed in Tallahassee, Florida.

C. H. Fancy, P.E., Chief Bureau of Air Regulation

#### **CERTIFICATE OF SERVICE**

The undersigned duly designated deputy agency clerk hereby certifies that this INTENT TO ISSUE PSD PERMIT (including the PUBLIC NOTICE, Technical Evaluation and Preliminary Determination, Draft BACT Determination, and the DRAFT PSD permit) was sent by certified mail (\*) and copies were mailed by U.S. Mail before the close of business on | - | - OO to the person(s) listed:

John L. West, Stone Container Corp. \*

- C. Kirts, DEP NED
- J. Manning, RESD
- B. Oven, DEP-OSC
- D. Neely, EPA
- J. Bunyak, NPS
- D. Buff, Golder Associates
- D. Roberts, Esq., HGSS
- J. Antista, General Counsel, Fl Game & Fresh Water Fish Commission
- D. Russ, Esq., Dept. of Community Affairs
- E.M. Barker, Esq., Slott & Barker
- L.N. Curtin, Esq., Holland & Knight
- G.K. Radlinski, Esq., City of Jacksonville
- N.B. Barnard, Esq., St. Johns River Management District
- R. Vandiver, General Counsel, Fl Public Service Commission

Clerk Stamp.

FILING AND ACKNOWLEDGMENT FILED, on this date, pursuant to §120.52, Florida Statutes, with the designated Department Clerk, receipt of which is hereby acknowledged.

Tan John (Clerk)  $\frac{|-|-00}{(Date)}$ 

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se side?	SENDER:  Complete items 1 and/or 2 for additional services.  Complete items 3. 4a. and 4b.  Print your name and address on the reverse of this form so that we	can return this	I also wish to receive the following services (for an extra fee):		_
the reverse	<ul> <li>a Attach this form to the front of the mailpiece, or on the back if space does not permit.</li> <li>Write "Return Receipt Requested" on the mailpiece below the article number.</li> <li>The Return Receipt will show to whom the article was delivered and the date delivered.</li> </ul>		Addressee's Address     Restricted Delivery Consult postmaster for fee.		ipt Service
ADDRESS completed on	3. Article Addressed to:  John J. West Jen. Mgr.  Store Container  PD BOX 26998  Jackson Ville, FI	4b. Service ☐ Registere ☐ Express	$\frac{1}{1}$ $\frac{391}{1}$	916  Description Insured COD	using Return Recei
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ls your <u>B</u>	6. Signature: (Addressee or Agent)  X  PS Form 3811. December 1994 . 102	2595-98-B-0229	Domestic Ret	urn Receipt	-

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# NOTICE TO BE PUBLISHED IN THE NEWSPAPER

#### PUBLIC NOTICE OF INTENT TO ISSUE PSD PERMIT

## STATE OF FLORIDA DEPARTMENT OF ENVIRONMENTAL PROTECTION

DEP File No. 0310067-004-AC (PSD-FL-252)
Duval County, Florida

The Department of Environmental Protection (Department) gives notice of its intent to issue a permit under the requirements for the Prevention of Significant Deterioration of Air Quality (PSD permit) to Stone Container Corporation. The permit will allow an increase in the maximum steam production rate and heat input rate for each of the three existing package boilers at its Jacksonville Mill in Duval County, Florida. The three package boilers are operated to support the recycled paper mill operations. Each of the three package boilers will increase the steam production rate from 125,000 lb/hr to 150,000 lb/hr, but will maintain the current permitted emission levels for nitrogen oxides (NO<sub>x</sub>) and sulfur dioxide (SO<sub>2</sub>). Maximum heat input rate to each boiler will be 215 MMBtu/hr when firing natural gas, and 200 MMBtu/hr when firing No. 2 fuel oil. A Best Available Control Technology (BACT) determination was required for NO<sub>x</sub> pursuant to Rule 62-212.400, F.A.C.

The applicant's name and address are Stone Container Corporation, Post Office Box 26998, Jacksonville, Florida 32226-6998. The Jacksonville Mill is located at 9469 East Port Road, Jacksonville, Duval County, Florida.

 $NO_x$  emissions from the package boilers will be controlled through low- $NO_x$  burners and Flue Gas Recirculation.

The net emissions increase due to the increased steam production for PSD applicability purposes is summarized below (in tons per year).

Pollutant<br/>NOxNet Emissions Increase<br/>304PSD Significant Emission Rate<br/>40

An air quality impact analysis was conducted for  $NO_x$ . Emissions from the facility will not significantly contribute to or cause a violation of any state or federal ambient air quality standards.

The Department will accept written comments and requests for a public meeting concerning the proposed permit issuance action for a period of 30 (thirty) days from the date of publication of this "Public Notice of Intent to Issue PSD permit." Written comments and requests for a public meeting should be provided to the Department's Bureau of Air Regulation at 2600 Blair Stone Road, Mail Station #5505, Tallahassee, Florida 32399-2400. Any written comments filed shall be made available for public inspection.

The Department will issue the permit with the attached conditions unless a timely petition for an administrative hearing is filed pursuant to Sections 120.569 and 120.57 of the Florida Statutes. The petition must contain the information set forth below and must be filed (received) in the Office of General Counsel of the Department, 3900 Commonwealth Boulevard, Mail Station #35, Tallahassee, Florida 32399-3000. Petitions filed by the permit applicant or any of the parties listed below must be filed within fourteen (14) days of receipt of this notice of intent. Petitions filed by any persons other than those entitled to written notice under Section 120.60(3) of the Florida Statutes must be filed within fourteen days of publication of the public notice or within fourteen (14) days of receipt of this notice of intent, whichever occurs first. Under Section 120.60(3), however, any person who asked the Department for notice of agency action may file a petition within fourteen (14) days of receipt of that notice, regardless of

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the date of publication. A petitioner shall mail a copy of the petition to the applicant at the address indicated above at the time of filing. The failure of any person to file a petition within the appropriate time period shall constitute a waiver of that person's right to request an administrative determination (hearing) under Sections 120.569 and 120.57, Florida Statutes, or to intervene in this proceeding and participate as a party to it. Any subsequent intervention will be only at the approval of the presiding officer upon the filing of a motion in compliance with Rule 28-106.205 of the Florida Administrative

A petition that disputes the material facts on which the Department's action is based must contain the following information: (a) The name and address of each agency affected and each agency's file or identification number, if known; (b) The name, address and telephone number of the petitioner, the name, address, and telephone number of the petitioner's representative, if any which shall be the address for service purposes during the course of the proceeding; and explanation of how the petitioner's substantial interests will be affected by the agency determination; (c) A statement of how and when petitioner received notice of the agency action or proposed action; (d) A statement of all disputed issues of material facts. If there are none, the petition must so indicate; (e) A concise statement of the ultimate facts alleged, as well as the rules and statutes which entitle the petitioner to relief; and (f) A demand for relief.

A petition that does not dispute the material facts upon which the Department's action is based shall state that no such facts are in dispute and otherwise shall contain the same information as set forth above, as required by Rule 28-106.301 of the Florida Administrative Code.

Because the administrative hearing process is designed to formulate final agency action, the filing of a petition means that the Department's final action may be different from the petition taken by it in this notice. Persons whose substantial interests will be affected by any such final decision of the Department on the application have the right to petition to become a party to the proceeding, in accordance with the requirements set forth above.

A complete project file is available for public inspection during normal business hours, 8:00 a.m. to 5:00 p.m., Monday through Friday, except legal holidays, at:

Department of Environmental Protection Bureau of Air Regulation 111 South Magnolia Drive, Suite 4 Tallahassee, Florida 32301 Telephone: 850/488-1344 Fax: 850/922-6979

Northeast District Office 7825 Baymeadows Way, Suite 200B Jacksonville, Florida 32256-7590 Telephone: 904/448-4300 Fax: 904/448-4366

Department of Environmental Protection Regulatory & Environmental Services Department (RESD) Suite 225, 117 W. Duval Street Jacksonville, Florida 32202 Telephone: 904/630-3484 Fax: 904/630-3638

The complete project file includes the Draft Permit, the application and the information submitted by the responsible official, exclusive of confidential records under Section 403.111, Florida Statutes. Interested persons may contact the New Resource Review Section at 111 South Magnolia Drive, Suite 4, Tallahassee, Florida 32301, or call 850/488-0114, for additional information.

#### **TECHNICAL EVALUATION**

#### AND

#### PRELIMINARY DETERMINATION

#### STONE CONTAINER CORPORATION

Recycled Fiber Paper Mill Jacksonville, Duval County

DEP File No. 0310067-004-AC PSD-FL-252

Department of Environmental Protection Division of Air Resources Management Bureau of Air Regulation

January 5, 2000

#### 1. APPLICATION INFORMATION

#### 1.1 Applicant Name and Address

Stone Container Corporation (SCC)

9469 East Port Road

Jacksonville, Florida 32229

Authorized Representative: Mr. John L. West, General Manager

#### 1.2 Reviewing and Process Schedule

07-06-98:	Date of Receipt of Application
08-04-98:	DEP Completeness Request
09-09-98:	SCC's letter requesting additional time for response to DEP's Completeness
	Request of 08-04-98
08-12-99:	SCC's response to DEP's Completeness Request of 08-04-98
09-08-99:	DEP's 2 <sup>nd</sup> Completeness Request
09-10-99:	DEP's 3 <sup>rd</sup> Completeness Request
09-22-99:	DEP's 4 <sup>th</sup> Completeness Request
09-23-99:	SCC's response to DEP's Completeness Requests of 09-08-99
10-07-99:	SCC's response to DEP's Completeness Request of 09-22-99
12-07-99:	SCC's response to DEP's Completeness Request of 09-10-99. Application
	complete
01-xx-00:	Issue Intent

#### 2. FACILITY INFORMATION

#### 2.1 Facility Location

Stone Container Corporation (SCC) currently operates a 100-percent recycled fiber paper mill facility located in Jacksonville, Duval County. This site is approximately 61 kilometers from the Okeefenokee National Wilderness Refuge, a Class I PSD Area. The UTM coordinates of this facility are Zone 17; 442.4 km E; 3365.4 km N.

#### 2.2 Standard Industrial Classification Codes (SIC)

Major Group No.	26	`	Paper and Allied Products
Industry Group No.	2621		Paper Mills

#### 2.3 Facility Category

The facility has been operating as a 100-percent recycled fiber facility since 1992 in Jacksonville, Florida. Formerly, the facility had two bark boilers and three power boilers to provide steam to the paper making process. These five boilers were shut down in March, 1994, when the U.S. Generating Company Cedar Bay facility began commercial operation. The recycled fiber facility requires additional steam beyond that provided by the Cedar bay facility. As a result, three new package boilers were installed by SCC to provide this necessary steam.

The facility is classified as a major or Title V source of air pollution because emissions of at least one regulated air pollutant exceed 100 TPY. This industry is included in the list of the 28 Major Facility Categories per Table 62-212.400-1, F.A.C. Because emissions are greater than 100 TPY for at least one regulated air pollutant, the facility is classified as a major facility with respect to Rule 62-212.400, Prevention of Significant Deterioration (PSD). Per Table 62-212.400-2, modifications at the facility resulting in emissions increases greater than the listed significance levels require review per the PSD rules and a determination of Best Available Control Technology (BACT) per Rule 62-212, F.A.C. For the proposed changes, greater than significant increases will occur for NO<sub>x</sub>. As such, this pollutant is subject to review under the PSD permitting program.

#### 3. PROJECT DESCRIPTION

This permit addresses the following emissions units:

EMISSION UNIT NO.	System	Emission Unit Description
022	Process	Package Boiler No. 1
023	Process	Package Boiler No. 2
, 026	Process	Package Boiler No. 3

SCC currently operates a 100-percent recycled fiber paper mill located in Jacksonville, Florida. Three package boilers are operated to support the paper mill operations. The boilers are fired with natural gas or very low sulfur No. 2 fuel oil with a maximum sulfur content of 0.05 percent, by weight. The current maximum steam production for each boiler is 125,000 lb/hr steam. The current maximum heat input to each boiler is 174.7 MMBtu/hr when firing natural gas, and 164.5 MMBtu/hr when firing No. 2 fuel oil.

The Cedar Bay cogeneration facility currently supplies SCC with steam. However, the SCC recycle fiber facility at times requires additional steam beyond that provided by the Cedar Bay facility. SCC is proposing to increase the maximum steam rate and heat input rate to the boilers, while maintaining the current permitted emission levels. The Site Certification (PA88-24A) Conditions of Certification (COC) for Cedar Bay Cogeneration Project is also being modified. However, the only condition requiring modification is that related to SCC steam boiler emissions (Condition II.E), and that only so far as the limitation on steam rate for the SCC boilers (i.e., 375,000 lb/hr steam to be revised to 450,000 lb/hr steam). No change in emission limits contained in the COC is necessary or requested. The boilers currently have permitted allowable emission rates for nitrogen oxides (NO<sub>x</sub>) and sulfur dioxide (SO<sub>2</sub>). Each of the three package boilers will be rated at 150,000 lb/hr steam at 650 psig and 750°F. Maximum heat input to each boiler will be 215 MMBtu/hr when firing natural gas, and 200 MMBtu/hr when firing No. 2 fuel oil. Firing of No. 2 fuel oil will be limited to 10,750,000 gallons per year for all three boilers combined. This limit will insure SO<sub>2</sub> emissions do not exceed the PSD significance level of 40 tons per year.

#### TECHNICAL EVALUATION AND PRELIMINARY DETERMINATION

The proposed project will result in an increase in NOx emissions over and above the PSD significance level per Table 62-212.400-2, F.A.C. Therefore, PSD review is required for  $NO_x$ . None of the other pollutants are above the significant emission increases per Table 62-212.400-2, F.A.C., and will not undergo PSD review.

Estimated emissions from the proposed project are shown below:

POLLUTANT	EXISTING EMISSIONS (TPY)	PROPOSED EMISSIONS (TPY)	NET CHANGE IN EMISSIONS (TPY)	PSD REVIEW APPLIES?
PM	0.63	20.9	20.3	No
PM <sub>10</sub>	0.63	15.5	14.9	No
SO <sub>2</sub>	0.08	39.8	39.7	No
NO <sub>x</sub>	6.28	310	303.7	Yes
СО	2.62	58.4	55.8	No
VOC	0.18	3.88	3.70	No
Pb	3.40E-05	0.0072	0.0072	No
Hg	1.88E-08	0.0022	0.0022	No
F	0.0	0.024	0.024	No
SAM	0.0	0.66	0.66	No

#### 4. RULE APPLICABILITY

The proposed project is subject to permitting, preconstruction review, emissions limits and compliance requirements under the provisions of Chapter 403, Florida Statutes, and Chapters 62-4, 62-204, 62-210, 62-212, 62-296, and 62-297 of the Florida Administrative Code (F.A.C.).

This facility is located in Duval County; an area designated as attainment for all criteria pollutants in accordance with Rule 62-204.360, F.A.C. The proposed project is subject to review under Rule 62-212.400, F.A.C., Prevention of Significant Deterioration (PSD), because the potential emission increases for NO<sub>x</sub> exceeds the significant emission rate given in Chapter 62-212, Table 62-212.400-2, F.A.C. PSD review requires an assessment of air quality impacts and a determination of Best Available Control Technology (BACT).

The emission units affected by this permit modification shall comply with all applicable provisions of the Florida Administrative Code (including applicable portions of the Code of Federal Regulations incorporated therein) and, specifically, the following Chapters and Rules:

#### TECHNICAL EVALUATION AND PRELIMINARY DETERMINATION

Chapter 62-4	Permits.
Rule 62-204.220	Ambient Air Quality Protection
Rule 62-204.240	Ambient Air Quality Standards
Rule 62-204.260	Prevention of Significant Deterioration Increments
Rule 62-204.360	Designation of Prevention of Significant Deterioration Areas
Rule 62-204.800	Federal Regulations Adopted by Reference
Rule 62-210.300	Permits Required
Rule 62-210.350	Public Notice and Comments
Rule 62-210.370	Reports
Rule 62-210.550	Stack Height Policy
Rule 62-210.650	Circumvention
Rule 62-210.700	Excess Emissions
Rule 62-210.900	Forms and Instructions
Rule 62-212.300	General Preconstruction Review Requirements
Rule 62-212.400	Prevention of Significant Deterioration
Rule 62-213	Operation Permits for Major Sources of Air Pollution
Rule 62-296.320	General Pollutant Emission Limiting Standards
Rule 62-297.310	General Test Requirements
Rule 62-297.401	Compliance Test Methods
Rule 62-297.520	EPA Continuous Monitor Performance Specifications

#### 5. SOURCE IMPACT ANALYSIS

#### 5.1 Air Quality Analysis

#### 5.1.1 Introduction

The proposed project will result in a net increase in emissions of NO<sub>2</sub> at levels in excess of PSD significant amounts. The air quality impact analyses required by the PSD regulations for this pollutant includes:

- A significant impact analysis;
- An analysis of existing air quality;
- An Ambient Air Quality Standards (AAQS) analysis;
- A PSD increment analysis;
- An analysis of impacts on soils, vegetation, and visibility and of growth-related air quality modeling impacts.

For  $NO_x$  the significant impact analyses performed by the applicant predicted maximum off-site impacts of greater than the significance level of 1  $\mu$ g/m³, annual average, in the vicinity of the facility but less than 0.1  $\mu$ g/m³, annual average, at the PSD Class I areas. As a result, the applicant was required to perform a PSD Class II Increment Analysis, an AAQS Analysis, and an Additional Impact Analysis at the PSD Class I areas.

Based on the required analyses, the Department has reasonable assurance that the proposed project, as described in this report and subject to the conditions of approval proposed herein, will

not cause or significantly contribute to a violation of any AAQS (there is no PSD increment for CO). However, the following EPA-directed stack height language is included: "In approving this permit, the Department has determined that the application complies with the applicable provisions of the stack height regulations as revised by EPA on July 8, 1985 (50 FR 27892). Portions of the regulations have been remanded by a panel of the U.S. Court of Appeals for the D.C. Circuit in NRDC v. Thomas, 838 F. 2d 1224 (D.C. Cir. 1988). Consequently, this permit may be subject to modification if and when EPA revises the regulation in response to the court decision. This may result in revised emission limitations or may affect other actions taken by the source owners or operators." A discussion of the required analyses follows.

#### 5.1.2 Analysis of Existing Air Quality and Determination of Background Concentrations

Preconstruction ambient air quality monitoring is required for all pollutants subject to PSD review unless otherwise exempted or satisfied. The monitoring requirement may be satisfied by using existing representative monitoring data, if available. An exemption to the monitoring requirement may be obtained if the maximum air quality impact resulting from the projected emissions increase, as determined by air quality modeling, is less than a pollutant-specific *de minimis* concentration. In addition, if EPA has not established an acceptable monitoring method for the specific pollutant, monitoring may not be required.

If preconstruction ambient monitoring is exempted, determination of background concentrations for PSD significant pollutants with established AAQS may still be necessary for use in any required AAQS analysis. These concentrations may be established from the required preconstruction ambient air quality monitoring analysis or from existing representative monitoring data. These background ambient air quality concentrations are added to pollutant impacts predicted by modeling and represent the air quality impacts of sources not included in the modeling.

The table below shows that the maximum predicted NO<sub>2</sub> impact from the project is predicted to be less than the monitoring *de minimis* level. Therefore, preconstruction ambient air quality monitoring is not required for this pollutant.

# Maximum Project NO<sub>2</sub> Air Quality Impact for Comparison to the Monitoring de Minimis Level.

Averaging Time	Max Predicted Impact (ug/m <sup>3</sup> )	De Minimis Level (ug/m <sup>3</sup> )	Impact Greater Than de Minimis?	
Annual	1.23	14	No	

#### 5.1.3 Models and Meteorological Data Used in the Air Quality Impact Analysis

The applicant and the Department used the EPA-approved Industrial Source Complex Short-Term (ISCST3) dispersion model to evaluate the pollutant emissions from the proposed project. The model determines ground-level concentrations of inert gases or small particles emitted into the

#### TECHNICAL EVALUATION AND PRELIMINARY DETERMINATION

atmosphere by point, area, and volume sources. The model incorporates elements for plume rise, transport by the mean wind, Gaussian dispersion, and pollutant removal mechanisms, such as deposition. The ISCST3 model allows for the separation of sources, building wake downwash, and various other input and output features. A series of specific model features, recommended by the EPA, are referred to as the regulatory options. The applicant used the EPA recommended regulatory options. Direction-specific downwash parameters were used for all sources for which downwash was considered. The stacks associated with this project all satisfy the good engineering practice (GEP) stack height criteria.

Meteorological data used in the ISCST3 model consisted of a consecutive 5-year period of hourly surface weather observations and twice-daily upper air soundings from the National Weather Service (NWS) stations at Jacksonville International Airport, Florida (surface data) and Waycross, Georgia (upper air data). The 5-year period of meteorological data was from 1983 through 1987. These NWS stations were selected for use in the study because they are the closest primary weather stations to the study area and are most representative of the project site. The surface observations included wind direction, wind speed, temperature, cloud cover, and cloud ceiling.

Since five years of data were used in ISCST3, the highest-second-high (HSH) short-term predicted concentrations were compared with the appropriate AAQS. For determining the project's significant impact area in the vicinity of the facility, and if there are significant impacts from the project on any PSD Class I area, the highest short-term predicted concentration were compared to the significant impact level.

#### 5.1.4 Significant Impact Analysis

Initially, the applicant conducts modeling using only the proposed project's emissions changes. If this modeling shows significant impacts, further modeling is required to determine the project's impacts on any applicable AAQS and PSD increments. The SCC facility is located in a PSD Class II area. A total of 350 receptors were used in the significant impact analysis. These receptors were placed along 36 polar radials spaced 10 degrees apart and centered on SCC's package boilers. The innermost receptors along each radial were located on the plant property boundary. An additional 134 off-property receptors were located at distances of 0.4, 0.6, 0.8, 1.0 and 1.2 kilometers from the origin to cover the area between the property boundary and the closest regular receptor grid distance of 1.5 km. Additional regular receptors were located offsite along each radial at distances of 2.0, 3.0, 4.0 and 5.0 kilometers from the modeling origin.

In addition, eleven discrete receptors were used to predict NO<sub>2</sub> impacts at the two closest PSD Class I areas. Ten of the 11 receptors were located along the southern and eastern boundaries of the Okeefenokee National Wilderness Refuge (ONWR) located approximately 160 kilometers (km) northwest of the facility. One additional receptor was located at the Wolf Island National Wilderness Refuge (WINWR), located approximately 100 km north of the facility.

The tables below summarize the results of this modeling. The maximum predicted air quality impacts due to NO<sub>x</sub> emissions from the proposed project are greater than the significant impact level in the vicinity of the facility. Therefore, the applicant was required to do further NO<sub>2</sub>

modeling in the vicinity of the facility, within the applicable significant impact area, to determine the impact of the project along with all other sources in the vicinity of the facility. The significant impact area is based upon the predicted radius of significant impact. The maximum predicted air quality impact due to NO<sub>x</sub> emissions is less than the significant impact level in the Class I areas; therefore, no further Class I modeling was required

MAXIMUM PROJECT AIR QUALITY IMPACT FOR COMPARISON TO THE PSD CLASS II SIGNIFICANT IMPACT LEVEL IN THE VICINITY OF THE							
	FACILITY						
Pollutant	Predicted Impact Level Impact Significant Significant						
NO <sub>2</sub>	Annual	1.23	1	Yes	0.6		

MAXIMUM PROJECT IMPACT IN THE OKEFENOKEE AND WOLF ISLAND NWA'S FOR COMPARISON TO THE PSD CLASS I SIGNIFICANT IMPACT LEVEL							
	SIGNIF		,				
	Maximum   Significant   Significant						
	Predicted Impact Level Impact						
Pollutant							
	Time (μg/m³)						
NO <sub>2</sub>	Annual	0.009	0.1	No			

#### 5.1.5 Compliance with AAQS and PSD Increments

The PSD increment represents the amount that new sources in an area may increase ambient ground level concentrations of a pollutant. The results of the PSD Class II increment analysis presented in the table below show that the maximum predicted multi-source impact is less than the allowable Class II increment.

PSD CLASS II INCREMENT ANALYSIS					
Pollutant	Averaging Time	Maximum Predicted Impact (µg/m³)	Impact Greater than Allowable Increment (Yes/No)	Allowable Increment (µg/m³)	
NO <sub>2</sub>	Annual	<0.0>	No	25	

For pollutants subject to an AAQS review, the total impact on ambient air quality is obtained by adding a "background" concentration to the maximum modeled concentration. This "background"

#### TECHNICAL EVALUATION AND PRELIMINARY DETERMINATION

concentration takes into account all sources of a particular pollutant that are not explicitly modeled. The results of the AAQS analysis are summarized in the table below. As shown in this table, emissions from the proposed facility are not expected to cause or significantly contribute to a violation of any AAQS.

AMBIENT AIR QUALITY IMPACTS								
	Major Total							
	Sources Background Total Impact Florida							
	Averaging Impact Concentration Impact Greater AAQS							
Pollutant								
NO <sub>2</sub>	NO <sub>2</sub> Annual 11 28 39 No 100							

#### 5.2 Additional Impacts Analysis

#### 5.2.1 Impact Analysis Impacts On Soils, Vegetation, Visibility, and Wildlife

The maximum ground-level concentrations predicted to occur due to NOx emissions as a result of the proposed project, including all other nearby sources, will be below the associated AAQS. The AAQS are designed to protect both the public health and welfare. As such, this project is not expected to have a harmful impact on soils and vegetation in the PSD Class II area. An air quality related values (AQRV) analysis was done by the applicant for the Class I area. No significant impacts on this area are expected.

#### 5.2.2 Growth-Related Air Quality Impacts

The proposed modification will not significantly change employment, population, housing or commercial/industrial development in the area to the extent that a significant air quality impact will result.

#### 6. CONCLUSION

Based on the foregoing technical evaluation of the application and additional information submitted by the applicant, the Department has made a preliminary determination that the proposed project will comply with all applicable State of Florida and federal air pollution regulations, provided the Department's BACT determination is implemented.

Syed Arif, P.E. Cleve Holladay, Meteorologist

#### PERMITTEE:

Stone Container Corporation 9469 East Port Road Jacksonville, Florida 32229

Authorized Representative: Mr. John L. West, General Manager

**FID No.** 0310067

PSD No. PSD-FL-252

SIC No. 2621

**Project:** 3 Package Steam Boilers

Expires: January 31, 2001

### PROJECT AND LOCATION:

Permit for an increase in the maximum steam production rate for each package boiler at the Stone Container Corporation Recycled Fiber Paper Mill in Jacksonville. Each of the three package boilers will be rated at 150,000 lb/hr steam at 650 psig and 750°F. The project is located at 9469 East Port Road, Jacksonville, Duval County. The UTM coordinates of this facility are Zone 17; 442.4 km E; 3365.4 km N.

### STATEMENT OF BASIS:

This construction permit is issued under the provisions of Chapter 403 of the Florida Statutes (F.S.), and the Florida Administrative Code (F.A.C.) Chapters 62-4, 62-204, 62-210, 62-212, 62-296, and 62-297. The above named permittee is authorized to modify the facility in accordance with the conditions of this permit and as described in the application, approved drawings, plans, and other documents on file with the Department of Environmental Protection (Department).

### Attached appendices are made a part of this permit:

Appendix BD BACT Determination

Appendix GC Construction Permit General Conditions

Howard L. Rhodes, Director Division of Air Resources Management

### SECTION I. FACILITY INFORMATION

#### FACILITY DESCRIPTION

Stone Container Corporation (SCC) currently operates a 100-percent recycled fiber paper mill facility located in Jacksonville, Duval County. This site is approximately 61 kilometers from the Okeefenokee National Wilderness Refuge, a Class I PSD Area. The facility has been operating as a 100-percent recycled fiber facility since 1992 in Jacksonville, Florida. Formerly, the facility had two bark boilers and three power boilers to provide steam to the paper making process. These five boilers were shut down in March, 1994, when the U.S. Generating Company Cedar Bay facility began commercial operation. The recycled fiber facility requires additional steam beyond that provided by the Cedar Bay facility. As a result, three new package boilers were installed by SCC to provide this necessary steam.

SCC is proposing to increase the maximum steam rate and heat input rate to the boilers, while maintaining the current permitted emission levels. The boilers currently have permitted allowable emission rates for nitrogen oxides ( $NO_x$ ) and sulfur dioxide ( $SO_2$ ). Each of the three package boilers will be rated at 150,000 lb/hr steam at 650 psig and 750°F. Maximum heat input to each boiler will be 215 MMBtu/hr when firing natural gas, and 200 MMBtu/hr when firing No. 2 fuel oil. Firing of No. 2 fuel oil will be limited to 10,750,000 gallons per year for all three boilers combined. This limit will insure  $SO_2$  emissions do not exceed the PSD significance level of 40 tons per year.

The proposed project will result in an increase in  $NO_x$  emissions over and above the PSD significance level per Table 62-212.400-2, F.A.C. Therefore, PSD review is required for  $NO_x$ . None of the other pollutants are above the significant emission increases per Table 62-212.400-2, F.A.C., and will not undergo PSD review.

### REGULATORY CLASSIFICATION

The Stone Container facility is classified as a "Major or Title V Source" per Rule 62-210.200, F.A.C., because it has the potential to emit more than 100 tons per year of at least one regulated air pollutant.

This industry is included in the list of the 28 Major Facility Categories per Table 62-212.400-1, F.A.C. Because emissions are greater than 100 TPY for at least one regulated pollutant, the facility is a major facility with respect to Rule 62-212.400, Prevention of Significant Deterioration (PSD). Per Table 62-212.400-2, modifications at the facility resulting in emissions increases greater than the listed significance levels require review per the PSD rules and a determination of Best Available Control Technology (BACT) per Rule 62-212, F.A.C.

For the proposed changes, greater than significant increases will occur for  $NO_x$ . As such this pollutant is subject to review under the PSD permitting program.

### PERMIT SCHEDULE:

07-06-98:	Date of Receipt of Application
08-04-98:	DEP Completeness Request
09-09-98:	SCC's letter requesting additional time for response to DEP's
	Completeness Request of 08-04-98
08-12-99:	SCC's response to DEP's Completeness Request of 08-04-98
09-08-99:	DEP's 2nd Completeness Request
09-10-99:	DEP's 3rd Completeness Request
09-22-99:	DEP's 4th Completeness Request
09-23-99:	SCC's response to DEP's Completeness Requests of 09-08-99
10-07-99:	SCC's response to DEP's Completeness Request of 09-22-99
12-07-99:	SCC's response to DEP's Completeness Request of 09-10-99.
	Application complete
01-xx-00:	Issue Intent

#### **RELEVANT DOCUMENTS:**

The documents listed form the basis of the permit. They are specifically related to this permitting action. These documents are on file with the Department.

- Date of Receipt of Application: 07-06-98
- DEP's 1<sup>st</sup> Completeness Request: 08-04-98
- SCC's response to DEP's 1st Completeness Request: 08-12-99
- DEP's 2<sup>nd</sup> Completeness Request: 09-08-99
- DEP's 3<sup>rd</sup> Completeness Request: 09-10-99
- DEP's 4<sup>th</sup> Completeness Request: 09-22-99
- SCC's response to DEP's 2<sup>nd</sup> Completeness Request: 09-23-99
- SCC's response to DEP's 4<sup>th</sup> Completeness Request: 10-07-99
- SCC's response to DEP's 3<sup>rd</sup> Completeness Request: 12-07-99
- Application complete: 12-07-99
- Technical Evaluation and Preliminary Determination: 01-xx-00
- Best Available Control Technology determination (issued concurrently with permit)

### SECTION II. EMISSION UNIT(S) GENERAL REQUIREMENTS

- 1. Regulating Agencies: All documents related to applications for permits to operate, reports, tests, minor modifications and notifications shall be submitted to the Department's Northeast District Office, 7825 Baymeadows Way, Jacksonville, Florida 32256-7590 and Regulatory & Environmental Services Department (RESD) in Jacksonville. All applications for permits to construct or modify an emissions unit(s) subject to the Prevention of Significant Deterioration or Nonattainment (NA) review requirements should be submitted to the Bureau of Air Regulation (BAR), Florida Department of Environmental Protection (FDEP), 2600 Blair Stone Road (MS 5505), Tallahassee, Florida 32399-2400 (phone number 850/488-0114).
- 2. <u>General Conditions</u>: The owner and operator is subject to and shall operate under the attached General Permit Conditions G.1 through G.15 listed in *Appendix GC* of this permit. General Permit Conditions are binding and enforceable pursuant to Chapter 403 of the Florida Statutes. [Rule 62-4.160, F.A.C.]
- 3. <u>Terminology</u>: The terms used in this permit have specific meanings as defined in the corresponding chapters of the Florida Administrative Code.
- 4. <u>Forms and Application Procedures</u>: The permittee shall use the applicable forms listed in Rule 62-210.900, F.A.C. and follow the application procedures in Chapter 62-4, F.A.C. [Rule 62-210.900, F.A.C.]
- 5. Expiration: This air construction permit shall expire on January 31, 2001 [Rule 62-210.300(1), F.A.C.]. The permittee may, for good cause, request that this construction permit be extended. Such a request shall be submitted to the Bureau of Air Regulation prior to 60 days before the expiration of the permit. However, the permittee shall promptly notify the Department's Northeast District Office and RESD of any delays in completion of the project which would affect the startup day by more than 90 days. [Rule 62-4.090, F.A.C]
- 6. <u>Application for Title V Permit</u>: An application for a Title V operating permit, pursuant to Chapter 62-213, F.A.C., must be submitted to the Department's Northeast District Office and RESD. [Chapter 62-213, F.A.C.]
- 7. New or Additional Conditions: Pursuant to Rule 62-4.080(1), F.A.C., for good cause shown and after notice and an administrative hearing, if requested, the Department may require the permittee to conform to new or additional conditions. The Department shall allow the permittee a reasonable time to conform to the new or additional conditions, and on application of the permittee, the Department may grant additional time. [Rule 62-4.080(1), F.A.C.]
- 8. <u>Annual Reports</u>: Pursuant to Rule 62-210.370(3), F.A.C., Annual Operating Reports, the permittee is required to submit annual reports on the actual operating rates and emissions from this facility. Annual operating reports shall be sent to the Department's Northeast District Office and RESD by March 1<sup>st</sup> of each year. [Rule 62-210.370(3), F.A.C.]

### SECTION III. EMISSION UNIT(S) SPECIFIC CONDITIONS

The Specific Conditions listed in this section apply to the following emission units:

EMISSION UNIT NO.	System	Emission Unit Description
022	Process	Package Boiler No. 1
023	Process	Package Boiler No. 2
026	Process	Package Boiler No. 3

- 1. The construction and operation of these sources shall be in accordance with the capacities stated in the application dated June 1998. This permit shall replace PSD-FL-198(A).
- 2. The package boilers may each be operated continuously (8760 hrs/yr).
- 3. The maximum heat input rate to each boiler shall neither exceed 215 MMBtu/hr while firing natural gas nor 200 MMBtu/hr while firing No. 2 fuel oil.
- 4. In accordance with the terms of the Cedar Bay Cogeneration Project (CBCP) site certification, Stone Container Corporation (SCC) is limited to 640,000 lb/hr total steam consumption (380,000 lb/hr imported from CBCP and 260,000 lb/hr produced by SCC). When CBCP is not in operation or operating at reduced rates, SCC is permitted to produce up to 450,000 lb/hr steam and import up to 190,000 lb/hr from CBCP. This allows a maximum firing rate of 645 MMBtu/hr for all three package boilers when the CBCP facility is shutdown or operating at reduced rates.
- 5. The maximum allowable NO<sub>x</sub> emissions shall not exceed 0.2 lb/MMBtu, 34.94 lbs/hr and 153.1 tons/yr per boiler. The total NO<sub>x</sub> emissions from the three package boilers, in accordance with the terms of the CBCP site certification, shall not exceed 310 tons per year.
- 6. The three package boilers are permitted to fire both natural gas and No. 2 fuel oil, with the primary fuel being natural gas. The sulfur content of the No. 2 fuel oil shall not exceed 0.05 percent, by weight. Any delivery of No. 2 fuel oil shall be accompanied by a laboratory analysis quantifying the density and percent sulfur, by weight. Annual SO<sub>2</sub> emissions from No. 2 fuel oil firing, totaling all three boilers, shall not exceed 25 tons/year. In the event that the ceiling for SO<sub>2</sub> is expected to be exceeded due to unavailability of natural gas caused by factors beyond the control of SCC, SCC shall notify the Department that it anticipates exceeding the ceiling as provided herein; and, the emissions of SO<sub>2</sub> during the period of such curtailment shall not be counted against the yearly emissions ceiling of 25 tons unless administrative proceedings result in a finding that the exceedance was within SCC's control. In no event shall the total annual emissions of SO<sub>2</sub> from the three steam boilers exceed 41

### AIR CONSTRUCTION PERMIT 0310067-004-AC AND PSD-FL-252

tons/year. The notice shall include a statement or reasons for the request and supporting documentation, and shall be published by SCC, without supporting documents, in a newspaper of general circulation in Jacksonville, Florida, as defined in Section 403.5115(2), F.S. The filing and publication of the notice no later than 7 days following the date of exceedance, shall preclude any finding of violation by the Department until final disposition of any administrative proceedings.

- 7. Visible emissions (VE) shall not exceed 5 percent (%) opacity during natural gas firing and 10% opacity during fuel oil firing.
- 8. In accordance with the requirements of 40 CFR 60.48b(b), a continuous emission monitoring system (CEMs) for nitrogen oxides shall be installed, operated, and maintained. Also, the natural gas, fuel oil and steam flows (both from the package boilers and from the CBCP facility) shall be metered and continuously recorded. The data shall be logged daily and maintained so that it can be provided to the Department upon request.
- 9. Before this construction permit expires, each package boiler shall be tested and monitored for compliance with the emission limits in Specific Conditions No. 3, 5, 6 and 7. For the duration of all tests the emission units shall be operating at permitted capacity. Permitted capacity is defined as 90-100 percent of the maximum operating rate allowed by the permit. If it is impracticable to test at permitted capacity, then the emission unit may be tested at less than permitted capacity (i.e., 90 percent of the maximum operating rate allowed by the permit); in this case, subsequent emission unit operation is limited to 110 percent of the test load until a new test is conducted. Once the emission unit is so limited, then operation at higher capacities is allowed for no more than 15 consecutive days for the purposes of additional compliance testing to regain the permitted capacity in the permit.
- 10. Compliance tests for NO<sub>x</sub> shall be conducted in accordance with 40 CFR 60.46b(e)(4). Compliance with SO<sub>2</sub> limits shall be in accordance with 40 CFR 60.49b(r), and a stoichiometric quantification for SO<sub>2</sub> emissions shall be utilized using the actual density and sulfur weight percent and the quantity of fuel oil fired monthly. Compliance with visible emission limits shall be demonstrated initially and annually in accordance with EPA Method 9.
- 11. The Department's Northeast District office and the RESD (City of Jacksonville's Regulatory and Environmental Services Department) office shall be notified at least 15 days prior to the compliance tests. Compliance test results shall be submitted to the Department's Northeast District and Bureau of Air Regulation offices and the RESD office within 45 days after completion of the tests. Sampling facilities, methods and reporting shall be in accordance with 40 CFR 60.49b, Chapter 62-297 and 40 CFR 60, Appendix A.
- 12. The permittee, for good cause, may request that this construction permit be extended. Such a request shall be submitted to the Department's Bureau of Air Regulation prior to 60 days before the expiration of the permit. (Rule 62-4.090, F.A.C.)

13. Pursuant to 40 CFR 60.49b(r), quarterly reports shall be submitted to the RESD office (i.e., Administrator) certifying that only very low sulfur oil (i.e., ≤0.05% sulfur, by weight) meeting this definition was combusted in the affected facility during the preceding quarter. The firing of any fuel oil and its associated SO₂ emissions shall be quantified on a monthly and per boiler basis and submitted to the RESD office by the end of the month following the end of each quarter. The quarters are defined as January-March, April-June, July-September and October-December; also, and per boiler, the final quarterly report shall include the total amount of the fuel oil fired and the quantified associated SO₂ emissions for the year.

### Stone Container Corporation Recycled Fiber Paper Mill/ 3 Package Boilers PSD-FL-252 / 0310067-004-AC Jacksonville, Duval County

Stone Container Corporation (SCC) has applied to increase the maximum steam rate and heat input rate to the three package boilers. The boilers are operated to support the paper mill operations. The boilers are fired with natural gas or No. 2 fuel oil with a maximum sulfur content of 0.05 percent by weight. SCC is currently requesting an increase in the maximum steam production rate for each boiler from 125,000 lb/hr to 150,000 lb/hr steam. The Cedar Bay cogeneration facility that is located adjacent to the existing SCC facility provides part of the steam required for the recycle fiber facility. The recycle fiber facility requires additional steam beyond that provided by the Cedar Bay facility. SCC desires more flexibility in steam production in the case of a shutdown or curtailment by Cedar Bay. According to the terms of the Cedar Bay Site Certification proceedings, SCC is to be limited to a total steam consumption of 640,000 lb/hr, which includes 380,000 lb/hr, imported from the Cedar Bay facility. This leaves 260,000 lb/hr to be produced by the three package boilers under normal operating conditions. During periods when Cedar Bay facility is shut down or operating at reduced rates, SCC will be allowed to produce up to 450,000 lb/hr steam from the three package boilers and import up to 190,000 lb/hr steam from the Cedar Bay facility. The total steam consumption cap of 640,000 lb/hr for SCC will still be in place.

The project is subject to Prevention of Significant Deterioration (PSD) review for NO<sub>x</sub> in accordance with Rule 62-212.400, Florida Administrative Code (F.A.C.). A Best Available Control Technology (BACT) determination is part of the review required by Rules 62-212.400 and 62-296, F.A.C. Air pollution control equipment will consist of Low-NO<sub>x</sub> burners and flue gas recirculation to minimize NO<sub>x</sub> emissions from the 3 Package Boilers.

### **PROCESS EMISSIONS**

The applicant proposes the following emissions:

POLLUTANT	EXISTING EMISSIONS (TPY)	PROPOSED EMISSIONS (TPY)	NET CHANGE IN EMISSIONS (TPY)	PSD REVIEW APPLIES?
PM	0.63	20.9	20.3	No
PM <sub>10</sub>	0.63	15.5	14.9	No
SO <sub>2</sub>	0.08	39.8	39.7	No
NO <sub>x</sub>	6.28	310	303.7	Yes

Stone Container Corporation 3 Package Boilers

DEP File No. 0310067-004-AC

PSD-FL-252

POLLUTANT	EXISTING EMISSIONS (TPY)	PROPOSED EMISSIONS (TPY)	NET CHANGE IN EMISSIONS (TPY)	PSD REVIEW APPLIES?
CO	2.62	58.4	55.8	No
VOC	0.18	3.88	3.70	No
Pb	3.40E-05	0.0072	0.0072	No
Hg	1.88E-08	0.0022	0.0022	No
F	0.0	0.024	0.024	No
SAM	0.0	0.66	0.66	No

### DATE OF RECEIPT OF COMPLETE BACT APPLICATION:

December 7, 1999

### **BACT DETERMINATION PROCEDURE:**

In accordance with Chapter 62-212.400, F.A.C., this BACT determination is based on the maximum degree of reduction of each pollutant emitted which the Department of Environmental Protection (Department), on a case-by-case basis, taking into account energy, environmental and economic impacts, and other costs, determines is achievable through application of production processes and available methods, systems, and techniques. In addition, the regulations state that, in making the BACT determination, the Department shall give consideration to:

- Any Environmental Protection Agency determination of BACT pursuant to Section 169, and any emission limitation contained in 40 CFR Part 60 - Standards of Performance for New Stationary Sources or 40 CFR Part 61 - National Emission Standards for Hazardous Air Pollutants.
- All scientific, engineering, and technical material and other information available to the Department.
- The emission limiting standards or BACT determination of any other state.
- The social and economic impact of the application of such technology.

The EPA currently stresses that BACT should be determined using the "top-down" approach. The first step in this approach is to determine, for the emission unit in question, the most stringent control available for a similar or identical emission unit or emission unit category. If it is shown

that this level of control is technically or economically infeasible for the emission unit in question, then the next most stringent level of control is determined and similarly evaluated. This process continues until the BACT level under consideration cannot be eliminated by any substantial or unique technical, environmental, or economic objections.

### BACT EMISSION LIMITS PROPOSED BY APPLICANT:

POLLUTANT	EMISSION LIMIT	CONTROL TECHNOLOGY
NO <sub>x</sub>	0.2 lb/MMBtu, 34.94 lb/hr and 153.1 TPY	Low-NOx burners and FGR

### **BACT ANALYSIS**

### NITROGEN OXIDES (NO<sub>x</sub>)

Oxides of nitrogen ( $NO_x$ ) are generated during fuel combustion by oxidation of chemically bound nitrogen in the fuel (fuel  $NO_x$ ) and by thermal fixation of nitrogen in the combustion air (thermal  $NO_x$ ). As flame temperature increases, the amount of thermally generated  $NO_x$  increases. Fuel type affects the quantity and type of  $NO_x$  generated. Generally, natural gas is low in nitrogen. However it causes higher flame temperatures and generates more thermal  $NO_x$  than oil or coal, which have higher fuel nitrogen content, but exhibit lower flame temperatures.

NO<sub>x</sub> emissions represent a significant portion of the total emissions generated by this project, and must be minimized using BACT. A review of EPA BACT/LAER Clearinghouse (BACT Clearinghouse) information indicates that no boilers in the size range of the SCC boilers (i.e., 100-300 MMBtu/hr) which fire primarily natural gas have been required to install Selective Catalytic Reduction (SCR) or Selective Non-Catalytic Reduction (SNCR) as BACT. All have employed low-NO<sub>x</sub> burners and flue gas recirculation (FGR), which the SCC boilers employ.

The applicant has proposed combustion controls equipped on the three package boilers which includes FGR and low  $NO_x$  burners. The combination of FGR and low  $NO_x$  burners results in less  $NO_x$  formation. Low  $NO_x$  burners reduce  $NO_x$  by conducting the combustion process in stages. Staging partially delays the combustion process, resulting in a cooler flame which suppresses thermal  $NO_x$  formation.  $NO_x$  reductions of 40 to 85 percent (relative to uncontrolled emission levels) have been observed with low  $NO_x$  burners when combined with flue gas recirculation.

In a FGR system, a portion of the flue gas is recycled from the stack to the burner windbox. Upon entering the windbox, the cooler gas is mixed with combustion air prior to being fed to the burner. The FGR system reduces NO<sub>x</sub> emissions by two mechanisms. In the first mechanism, the recycled flue gas is made up of combustion products which acts as inerts during combustion of the fuel/air mixture. This additional mass is heated in the combustion zone, thereby lowering the peak flame temperature and reducing the amount of NO<sub>x</sub> formed. Second, to a lesser extent, FGR also reduces NO<sub>x</sub> formation by lowering the oxygen concentration in the primary flame zone. **This** 

combination of NO<sub>x</sub> controls and good combustion practices should provide effective emissions control.

### BACT DETERMINATION BY THE DEPARTMENT:

Based on the information provided by the applicant and the information searches conducted by the Department, lower emissions limits can be obtained employing the top-down BACT approach for NO<sub>x</sub>.

### NO<sub>x</sub> DETERMINATION

The top-down BACT approach for natural gas/fuel oil boilers listed in order from most stringent control to least:

- 1. Selective Catalytic Reduction (SCR)
- 2. Selective Noncatalytic Reduction (SNCR)
- 3. Good combustion design/practices

The following table summarizes the feasibility of using these control technologies with the Package Boilers as designed for installation in SCC Recycle Fiber Paper Mill.

Control Technology	Emission Reduction (%)	Technically Feasible	Cost per ton	Adverse Environ. Impacts
SCR with ammonia	80-90	Yes	\$4,600	Yes
SNCR	40-70	Yes	\$8,000	No
Low NO <sub>x</sub> Burners with Flue Gas Recirculation	20-50	Yes	N/A	No

Assuming maximum boiler operation, the cost per ton for SCR is about \$4,600/ton. Using a still very conservative annual capacity factor of 50 percent, the cost effectiveness increases to more than \$7,300/ton. This economic impact is very high considering that normally SCC's boilers will not operate or will operate at very reduced rates, since Cedar Bay will provide the majority of the steam to SCC. For NO<sub>x</sub> emissions, the Department accepts the applicants proposed use of low NO<sub>x</sub> burners with flue gas recirculation as BACT for this project.

The BACT emission level established by the Department is as follows:

POLLUTANT	EMISSION LIMIT
Nitrogen Oxides (NO <sub>x</sub> )	0.2 lb/mmBtu; 34.94 lb/hr and 153.1 TPY. Total NO <sub>x</sub> emissions from 3 package boilers is limited to 310 TPY.

### **COMPLIANCE**

Each package boiler shall be tested and monitored for compliance with the  $NO_x$  emission limits in accordance with 40 CFR 60.46b(e)(4).

### **DETAILS OF THE ANALYSIS MAY BE OBTAINED BY CONTACTING:**

Syed Arif, P.E., Permit Engineer Department of Environmental Protection Bureau of Air Regulation - MS 5505 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Recommended By:		Approved By:
C. H. Fancy, P.E., Chief		Howard L. Rhodes, Director
Bureau of Air Regulation		Division of Air Resources Management
	A Park of the Control	·
Date:		Date:

# GENERAL PERMIT CONDITIONS [F.A.C. 62-4.160]

- G.1 The terms, conditions, requirements, limitations, and restrictions set forth in this permit are "Permit Conditions" and are binding and enforceable pursuant to Sections 403.161, 403.727, or 403.859 through 403.861, Florida Statutes. The permittee is placed on notice that the Department will review this permit periodically and may initiate enforcement action for any violation of these conditions.
- G.2 This permit is valid only for the specific processes and operations applied for and indicated in the approved drawings or exhibits. Any unauthorized deviation from the approved drawings or exhibits, specifications, or conditions of this permit may constitute grounds for revocation and enforcement action by the Department.
- G.3 As provided in Subsections 403.087(6) and 403.722(5), Florida Statutes, the issuance of this permit does not convey and vested rights or any exclusive privileges. Neither does it authorize any injury to public or private property or any invasion of personal rights, nor any infringement of federal, state or local laws or regulations. This permit is not a waiver or approval of any other Department permit that may be required for other aspects of the total project which are not addressed in the permit.
- G.4 This permit conveys no title to land or water, does not constitute State recognition or acknowledgment of title, and does not constitute authority for the use of submerged lands unless herein provided and the necessary title or leasehold interests have been obtained from the State. Only the Trustees of the Internal Improvement Trust Fund may express State opinion as to title.
- G.5 This permit does not relieve the permittee from liability for harm or injury to human health or welfare, animal, or plant life, or property caused by the construction or operation of this permitted source, or from penalties therefore; nor does it allow the permittee to cause pollution in contravention of Florida Statutes and Department rules, unless specifically authorized by an order from the Department.
- G.6 The permittee shall properly operate and maintain the facility and systems of treatment and control (and related appurtenances) that are installed or used by the permittee to achieve compliance with the conditions of this permit, as required by Department rules. This provision includes the operation of backup or auxiliary facilities or similar systems when necessary to achieve compliance with the conditions of the permit and when required by Department rules.
- G.7 The permittee, by accepting this permit, specifically agrees to allow authorized Department personnel, upon presentation of credentials or other documents as may be required by law and at a reasonable time, access to the premises, where the permitted activity is located or conducted to:
  - (a) Have access to and copy and records that must be kept under the conditions of the permit;
  - (b) Inspect the facility, equipment, practices, or operations regulated or required under this permit, and,
  - (c) Sample or monitor any substances or parameters at any location reasonably necessary to assure compliance with this permit or Department rules.

Reasonable time may depend on the nature of the concern being investigated.

- G.8 If, for any reason, the permittee does not comply with or will be unable to comply with any condition or limitation specified in this permit, the permittee shall immediately provide the Department with the following information:
  - (a) A description of and cause of non-compliance; and
  - (b) The period of noncompliance, including dates and times; or, if not corrected, the anticipated time the non-compliance is expected to continue, and steps being taken to reduce, eliminate, and prevent recurrence of the non-compliance.

### GENERAL PERMIT CONDITIONS [F.A.C. 62-4.160]

The permittee shall be responsible for any and all damages which may result and may be subject to enforcement action by the Department for penalties or for revocation of this permit.

- G.9 In accepting this permit, the permittee understands and agrees that all records, notes, monitoring data and other information relating to the construction or operation of this permitted source which are submitted to the Department may be used by the Department as evidence in any enforcement case involving the permitted source arising under the Florida Statutes or Department rules, except where such use is prescribed by Sections 403.73 and 403.111, Florida Statutes. Such evidence shall only be used to the extent it is consistent with the Florida Rules of Civil Procedure and appropriate evidentiary rules.
- G.10 The permittee agrees to comply with changes in Department rules and Florida Statutes after a reasonable time for compliance, provided, however, the permittee does not waive any other rights granted by Florida Statutes or Department rules.
- G.11 This permit is transferable only upon Department approval in accordance with Florida Administrative Code Rules 62-4.120 and 62-730.300, F.A.C., as applicable. The permittee shall be liable for any non-compliance of the permitted activity until the transfer is approved by the Department.
- G.12 This permit or a copy thereof shall be kept at the work site of the permitted activity.
- G.13 This permit also constitutes:
  - (a) Determination of Best Available Control Technology (X)
  - (b) Determination of Prevention of Significant Deterioration (X); and
  - (c) Compliance with New Source Performance Standards (X).
- G.14 The permittee shall comply with the following:
  - (a) Upon request, the permittee shall furnish all records and plans required under Department rules. During enforcement actions, the retention period for all records will be extended automatically unless otherwise stipulated by the Department.
  - (b) The permittee shall hold at the facility or other location designated by this permit records of all monitoring information (including all calibration and maintenance records and all original strip chart recordings for continuous monitoring instrumentation) required by the permit, copies of all reports required by this permit, and records of all data used to complete the application or this permit. These materials shall be retained at least three years from the date of the sample, measurement, report, or application unless otherwise specified by Department rule.
  - (c) Records of monitoring information shall include:
    - 1. The date, exact place, and time of sampling or measurements;
    - 2. The person responsible for performing the sampling or measurements;
    - 3. The dates analyses were performed;
    - 4. The person responsible for performing the analyses;
    - 5. The analytical techniques or methods used; and
    - 6. The results of such analyses.
- G.15 When requested by the Department, the permittee shall within a reasonable time furnish any information required by law which is needed to determine compliance with the permit. If the permittee becomes aware that relevant facts were not submitted or were incorrect in the permit application or in any report to the Department, such facts or information shall be corrected promptly.

# Florida Department of Environmental Protection

TO:

Clair Fancy

FROM:

Syed Arif Sped Aug

DATE:

January 4, 2000

SUBJECT:

Stone Container Jacksonville Mill

PSD-FL-252; Three Package Boilers

Attached is the Public Notice and draft permit modification to increase the maximum steam production rate and heat input rate for each of the three existing package boilers at their recycled paper mill in Jacksonville, Florida. The steam production rate for each boiler will increase from 125,000 lb/hr to 150,000 lb/hr while maintaining their current permitted emission levels for  $NO_x$  and  $SO_2$ .

A Best Available Control Technology determination was required for NO<sub>x</sub> pursuant to Rule 62-212.400, F.A.C. NO<sub>x</sub> emissions will be controlled through low-NOx burners and flue gas recirculation.

I recommend your approval and signature.

SA/a

Attachments



# Department of **Environmental Protection**

Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

David B. Struhs Secretary

## P.E. Certification Statement

Permittee:

**Stone Container Corporation** Recycled Fiber Paper Mill 3 Package Boilers

**DEP File No.:** 

0310067-004-AC

Permit No.:

PSD-FL-252

**Project type:** Air Construction Permit for increase in the maximum steam rate and heat input rate to each of the three existing package boilers, while maintaining the current permitted emission levels. NO<sub>x</sub> emissions will be minimized by Low-NO<sub>x</sub> burners and Flue Gas recirculation.

I HEREBY CERTIFY that the engineering features described in the above referenced application and subject to the proposed permit conditions provide reasonable assurance of compliance with applicable provisions of Chapter 403, Florida Statutes, and Florida Administrative Code Chapters 62-4 and 62-204 through 62-297. However, I have not evaluated and I do not certify aspects of the proposal outside of my area of expertise (including but not limited to the electrical, mechanical, structural, hydrological, and geological features).

Registration Number: 51861

Department of Environmental Protection Bureau of Air Regulation New Source Review Section 111 South Magnolia Drive, Suite Tallahassee, Florida 32301 Phone (850) 921-9528 Fax (850) 922-6979

#### Golder Associates Inc.

6241 NW 23rd Street, Suite 500 Gainesville, FL 32653-1500 Telephone (352) 336-5600 Fax (352) 336-6603



December 6, 1999

9837525

Florida Department of Environmental Protection Bureau of Air Regulation 2600 Blair Stone Road Tallahassee, FL 32399-2400 RECEIVED
DEC 07 1999

BUREAU OF AIR REGULATION

Attention: Mr. A. A. Linero, P.E.

RE: STONE CONTAINER CORPORATION

DEP FILE NO. 0310067-004-AC (PSD-FL-252)

RECYLCED FIBER FACILITY - INCREASE IN STEAM RATE

Dear Mr. Linero:

This letter is in regard to Stone Container Corporation's (SCC) request to increase the steam production rate from the Package Boiler Nos. 1, 2, and 3 located at their Jacksonville recycled fiber facility. Specifically, SCC requests an increase in the steam production rate for each package boiler from 125,000 pounds per hour (lb/hr) to 150,000 lb/hr without increasing the pollutant emission rates above the current allowable limits.

On September 8, 1999, the Department issued a second completeness letter (the initial completeness letter was issued August 4, 1998, and not responded to by SCC until recently) requesting additional information to process SCC's request. The Department subsequently issued a third completeness letter dated September 10, 1999, referencing concerns expressed in a letter from Richard L. Robinson from the City of Jacksonville's Regulatory & Environmental Services Department, Air and Water Quality Division (AWQD). Mr. Robinson requested that Stone Container Corporation provide reasonable assurance that compliance could be demonstrated with NO<sub>X</sub> emission limits for the package boilers at a heat input rate for each unit of 215 MMBtu/hr.

On September 22, 1999, in a letter prepared by Golder Associates Inc. (Golder), SCC responded to the Department's completeness inquiries. Golder's letter specifically addressed the two items presented in the Department's letter dated September 8, 1999, and requested permission to perform additional  $NO_X$  testing at the higher steam production rate to alleviate Mr. Robinson's concerns. On September 30, 1999, SCC received permission from the City of Jacksonville to perform the requested source tests. A clarification letter was issued by the AWQD on October 5, 1999, authorizing simultaneous operation of the package boilers at steam production rates of 150,000 lb/hr each.

The purpose of this letter is to present the results of the additional source testing preformed at the requested steam production rate. These results have already been

submitted to the City of Jacksonville AWQD. Please find the attached tables summarizing the steam production rate (1,000 lb/hr), heat input rate (MMBtu/hr), and  $NO_x$  emission rate (lb/MMBtu).  $NO_x$  emission rates for the package boilers were measured using the existing continuous monitoring system during a 3-day period from October 20, through October 23, 1999. As shown in the attached table, each of the boilers were brought up from a cold start at 5 p.m. on October 20. Generally, the heat input rates were increased until each boiler was operating at a steam production rate of approximately 150,000 lb/hr. The boilers were maintained at a steam production rate of approximately 150,000 lb/hr for approximately 40 hours before the heat input rate was decreased. The package boilers were shut down at 4 p.m. on October 23.  $NO_x$  emission rates were measured during start up, shut down, and normal operation.

The maximum  $NO_X$  emission rate measured during the test period was 0.139 lb/MMBtu at a steam production rate of 142,000 lb/hr. The maximum  $NO_X$  emission rate measured during operation at a steam production capacity of 150,000 lb/hr was 0.135 lb/MMBtu. These measured emission rates are well below the current  $NO_X$  emission limit for the package boilers of 0.2 lb/MMBtu.

The maximum heat input rate recorded during the test period was 191 MMBtu/hr at steam production rates from 144,000 to 150,000 lb/hr. Although the package boilers did not operate as high as 215 MMBtu, this is merely an indication that the boilers were operating at better than design efficiency during the test. Due to the variability of boiler operation, SCC continues to request that the boilers be permitted to operate at a maximum heat input rate of 215 MMBtu/hr, if necessary.

If you have any questions concerning the information presented in this letter, please call me at your convenience.

CC: S. any, BAK NED C. Holladay, BAR EPA NPS

Sincerely,

\_GOLDER ASSOCIATES INC.

Enclosures

cc: J. Eskridge, SCC T. Cole, OHFC

 $\label{locality} $$\GATORBAIT\DP\Projects\98\9837525a\03\\#03\tr.doc$$ 

		В	OILER 1			BOILER 2				BOILER 3 .			
	STEAM	NA	TGAS	Nox	STEAM	NA	T GAS	Nox	STEAM	NA	T GAS	Nox	
TIME	KLB/HR	SCFM	mmBtu/hr	Lbs/mmBtu	KLB/HR	SCFM	mmBtu/hr	Lbs/mmBtu	KLB/HR	SCFM	mmBtu/hr	Lbs/mmBtu	
7:00	0	0	0	0	0	0	0	0	0	0	0	0	
8:00	0	0	0	0	0	0	0	0	0	0	0	. 0	
9:00	0	0	0	0	0	0	0	0	0	0	0	0	
10:00	0	0	0	0	0	0	0.	0	0	0	0	0	
11:00	0	0	0	0	0	0	0	0	0	0	0	. 0	
12:00	0	0	0	0	0	0	0	0	0	0	0	0	
13:00	0	0	0	0	0	0	0	0	0	0	0	0	
14:00	0	0	0	0	0	. 0	0	0	0	0	0	0	
15:00	0	0	0	0	0	0	0	0	0	0	0	0	
16:00	0	0	0	0	0	0	0	0	0	0	0	0	***************************************
17:00	0	0	0	0.059	0	0	0	0.025	0	0	0	0.076	
18:00	31	920	58	0.092	42	796	50	0.053	9	438	28	0.100	
19:00	116	2318	146	0.087	107	2214	139	0.058	110	2278	144	0.078	
20:00	122	2436	153	0.088	123	2581	163	0.059	137	2793	176	0.075	
21:00	122	2440	154	0.087	123	2580.	163	0.058	136	2790	176	0,076	
22:00	121	2445	154	0.086	122	2579	162	0.057	135	2787	176	0.076	
23:00	121	2443	154	0.088	123	2576	162	0.058	136	2776	175	0.078	
0:00	121	2441	154	0.088	122	2574	162	0.058	135	2769	174	0.078	
1:00	120	2439	154	0.088	122	2571	162	0.058	135	2767	174	0.078	
2:00	121	2438	154	0.089	123	2568	162	0.059	136	2757	174	0.079	
3:00	121	2437	154	0.090	123	2567	162	0.059	136	2766	174	0.080	
4:00	121	2437	154	0.089	123	2566	162	0.059	136	2772	175	0.080	
5:00	121	2434	153	0.089	123	2566	162	0.059	135	2760	174	0.080	
6:00	95	2028	128	0.091	111	2380	150	0.058	136	2747	173	0.081	

	i -i		OILER 1				OILER 2	i	BOILER 3 .				
	STEAM	NA	TGAS	Nox	STEAM	NA	T GAS	Nox	STEAM	NA	T GAS	Nox	
IME	KLB/HR	SCFM	mmBtu/hr	Lbs/mmBtu	KLB/HR	SCFM	mmBtu/hr	Lbs/mmBtu	KLB/HR	SCFM	mmBtu/hr	Lbs/mmBtu	
7:00	56	1110	70	0.094	77	1418	89	0.065	140	2756	174	0.084	
8:00	55	1076	68	0.089	62	1085	68	0.066	140	2752	173	0.084	
9:00	56	1076	68	0.089	62	1083	68	0.067	140	2748	173	0.080	
10:00	56	1077	68	0.094	62	1087	68	0.056	140	2766	174	0.079	
11:00	55	1084	68	0.093	63	1101	69	0.057	140	2757	174	0.080	
12:00		41	3		99	1944	122	0.064	140	2755	174	0.081	
13:00	43	1033	65	0.083	76	1462	92	0.064	140	2753	173	0.081	
14:00	143	2888	182	0.085	17	223	14	T	138	2758	174	0.082	
15:00	143	2925	184	0.086	99	2066	130	0.068	94	1906	120	0.086	
16:00	143	2925	184	0.085	142	2896	182	0.072	0	0	0		
17:00	142	2932	185	0.085	146	2813	177	0.081	20	610	38		
18:00	142	2939	185	0.085	141	2781	175	0.080	130	2626	165	0.082	
19:00	140	2937	185	0.085	140	2776	175	0.080	141	2764	174	0.086	
20:00	142	2937	185	0.086	134	2775	175	0.081	143	2765	174	0.086	****
21:00	135	2936	185	0.086	141	2773	175	0.081	144	2761	174	0.087	
22:00	136	2932	185	0.085	142	2771	175	0.081	144	2766	174	0.086	
23:00	86	1800	113	0.096	95	1715	108	0.088	149	2765	174	0.088	
0:00	78	1527	96	0.100	95	1640	103	0.089	148	2746	173	0.090	
1:00	83	1605	101	0.095	97	1663	105	0.091	149	2701	170	0.090	
2:00	97	2096	132	0.093	109	2037	128	0.088	146	2670	168	0.089	
3:00	125	2888	182	0.089	136	2773	175	0.084	144	2668	168	0.087	
4:00	143	2885	182	0.088	143	2713	171	0.083	144	2699	170	0.085	
5:00	145	2879	181	0.090	145	2705	170	0.084	145	2703	170	0.086	
6:00	145	2876	181	0.090	145	2704	170	0.085	145	2696	170	0.087	

	!	B	OILER 1	i	BOILER 2				BOILER 3 .				
	STEAM NA		T GAS	Nox	STEAM	NAT GAS		S Nox	STEAM	NA	T GAS	Nox	
TIME	KLB/HR	SCFM	mmBtu/hr	Lbs/mmBtu	KLB/HR	SCFM	mmBtu/hr	Lbs/mmBtu	KLB/HR	SCFM	mmBtu/hr	Lbs/mmBtu	
7:00	145	2876	181	0.090	145	2705	170	0.083	145	2695	170	0.088	
8:00	145	2875	181	0.088	145	2704	170	0.083	145	2696	170	0.089	
9:00	145	2876	181	0.088	146	2704	170	0.080	146	2695	170	0.091	
10:00	145	2881	182	0.087	145	2705	170	0.081	146	2699	170	0.091	
11:00	146	2913	184	0.090	144	2709	171	0.084	145	2705	170	0.094	
12:00	148	2966	187	0.092	143	2712	171	0.086	144	2710	171	0.095	
13:00	150	3011	190	0.106	142	2714	171	0.084	143	2711	171	0.095	
14:00	150	3015	190	0.110	143	2714	171	0.085	144	2718	171	0.094	
15:00	149	3022	190	0.111	147	2869	181	0.127	146	2862	180	0.121	
16:00	150	3022	190	0.110	149	3019	190	0.135	144	3026	191	0.127	
17:00	150	3021	190	0.110	149	3018	190	0.136	149	3027	191	0.127	
18:00	150	3019	190	0.110	150	3017	190	0.135	150	3024	191	0.127	
19:00	150	3018	190	0.110	150	3018	190	0.135	150	3022	190	0.127	
20:00	150	3014	190	0.111	150	3016	190	0.134	150	3013	190	0.127	
21:00	150	3013	190	0.111	149	3016	190	0.134	149	3009	190	0.128	
22:00	149	3012	190	0.111	149	3016	190	0.133	143	3005	189	0.128	
23:00	146	3001	189	0.112	149	3017	190	0.135	149	3006	189	0.129	
0:00	145	2921	184	0.114	150	3020	190	0.135	150	3007	189	0.128	
1:00	134	2921	184	0.114	150	3021	190	0.135	149	2993	189	0.129	
2:00	140	2924	184	0.115	150	3022	190	0.135	148	2991	188	0.131	
3:00	147	2923	184	0.115	149	3022	190	0.136	150	3010	190	0.130	
4:00	147	2923	184	0.114	149	3023	190	0.134	149	3009	190	0.129	
5:00	147	2924	184	0.115	149	3023	190	0.135	149	3012	190	0.130	
6:00	148	2962	187	0.114	148	3022	190	0.134	149	3009	190	0.130	

		В	OILER 1			BOILER 2				BOILER 3 .			
*	STEAM	NA	T GAS	Nox	STEAM	NA	T GAS	Nox	STEAM	NA	T GAS	Nox	
TIME	KLB/HR	SCFM	mmBtu/hr	Lbs/mmBtu	KLB/HR	SCFM	mmBtu/hr	Lbs/mmBtu	KLB/HR	SCFM	mmBtu/hr	Lbs/mmBtu	
7:00	146	2971	187	0.114	146	3021	190	0.135	147	3009	190	0.131	
8:00	144	2856	180	0.114	147	3021	190	0.133	148	3004	189	0.131	
9:00	138	2730	172	0.113	144	2862	180	0.134	146	2835	179	0.136	
10:00	139	2733	172	0.105	141	2634	166	0.129	142	2720	171	0.139	
11:00	144	2823	178	0.102	141	2644	167	0.115	76	1450	91	0.079	
12:00	144	2836	179	0.101	139	2537	160	0.097	127	2336	147	0.080	
13:00	144	2839	179	0.101	140	2537	160	0.097	125	2335	147	0.083	
14:00	103	1964	124	0.114	109	1798	113	0.107	90	1584	100	0.092	
15:00	88	1860	117	0.125	109	1819	115	0.105	25	562	35	0.103	
16:00	7	189	12		37	487	31	0.071	39	716	45	0.133	
17:00													
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#### Golder Associates Inc.

6241 NW 23rd Street, Suite 500 Gainesville, FL 32653-1500 Telephone (352) 336-5600 Fax (352) 336-6603



October 6, 1999

RECEIVED

Florida Department of Environmental Protection Bureau of Air Regulation 2600 Blair Stone Road Tallahassee, FL 32399-2400 OCT 07 1999

**BUREAU OF AIR REGULATION** 

Attention: Mr. A. A. Linero, P.E.

RE: Stone Container Corporation - Jacksonville

DEP File No. 0310067-004-AC (PSD-FL-252) Recycled Fiber Facility – Increase in Steam Rate

Dear Mr. Linero:

Stone Container Corporation (SCC) has received the Department's letter dated September 22, 1999, regarding SCC's proposed steam rate increase for the three steam boilers located at the Jacksonville recycle fiber mill. This letter included a memo from the U.S. Fish & Wildlife Service (USFWS), which contained additional comments on SCC's PSD permit application. Each of the USFWS's comments are addressed below, in the same order as they appear in their letter.

- 1. The original application that SCC made to the Department in July 1998 acknowledged that PSD review applied to the proposed project. The application presented the elements of PSD review, i.e., air impact analysis, BACT evaluation, additional impact analysis, etc. Possibly the USFWS has discarded the original application, since it was submitted nearly a year ago.
- 2. Regarding the SCR cost analysis, the analysis has been revised to incorporate the suggested changes. Structural costs have been eliminated from the purchased equipment costs and are now included in the direct installation costs. Indirect capital costs were based on the purchased equipment costs. Working capital has been eliminated. The interest rate has been revised to reflect 7 percent. These and other factors have been adjusted to be more consistent with the Cost Control manual.

The revised cost analysis is presented in Table 1R attached. As shown, the cost effectiveness decreases slightly to about \$4,600/ton of  $NO_x$  removed, assuming maximum boiler operation. Using a still very conservative annual capacity factor of 50 percent, the cost effectiveness increases to more than \$7,300/ton. This economic impact is very high considering that normally SCC's boilers will not operate or will operate at very reduced loads, since the majority of steam needs will provided by Cedar bay. Considering SCC's normal operating mode, the costs of applying SCR to these boilers is economically infeasible.

Thank you for consideration of these comments. Please call if you have any questions concerning this matter.

Sincerely,

GOLDER ASSOCIATES INC.

David a Buff

David A. Buff, P.E.

Principal Engineer

Florida P.E. #19011

SEAL

DB/arz

cc: Joe Eskridge

Terry Cole

Buck Oven, FDEP-OSC

J. Manning, RESD

P:\Projects\98\9837525a\02\#02-ltr.doc

CC: S. arif, BAR NEP C. Holladay, BAR EPA

NP5

Table 1. Cost Effectiveness for Us	ng SCR to Control NOx Emissions for Boiler Nos.1-3, Stone Container Corp. (revised	0/4/99)
------------------------------------	--	---------

			Maximum Operation		50% Operation	
Cost Items		Cost Factors	80% Removal	90% Removal	90% Removal	
Dog: Rema		Cost Factors	(1998 \$)	(1998 \$)	(1998 \$)	
DIRECT CAPITA	L COSTS (DCC):		\ <del>\</del>	( <del></del> <del></del> <del></del> <del> </del>	1	
(1) Purchase	ed Equipment Cost					
(a) Basi	c Equipment/Services	Based on Vendor Quote (c)	1,050,000	1,200,000	1,200,00	
(b) Instr	umentation	0.10 x 1a	105,000	120,000	120,00	
	onia Storage Tank	\$140 per 1000 lb mass flow	84,000	84,000	84,00	
	ional Ductwork	Based on OAQPS Cost Control Manual, Ch. 10	120,000	120,000	120,00	
(e) Freig		0.05 x 1a	included	included	include	
	s Tax (Florida)					
	,	0.06 x (1a1e)	81,540	91,440	91,44	
(g) Subt		(1a1f)	1,440,540	1,615,440	1,615,44	
(2) Direct In	stallation (a)	0.30 x (1g)	432,162	484,632	484,63	
Total DCC:		(1g) + (2)	1,872,702	2,100,072	2,100,07	
IDIRECT CAPI	TAL COSTS (ICC): (a)					
	nstallation Costs					
` '	nology License Fee	Provided from Vendor Quote	included	included	include	
	neering & Supervision	Provided from Vendor Quote	included	included	include	
	struction & Field Expenses	(0.05) x (DCC)	93,635	105,004	105,00	
	struction Contractor Fee	(0.10) x (DCC)	187,270	210,007	210,00	
(e) Cont	ingencies	(0.25) x (DCC) - based on retrofit	468,176	525,018	525,01	
	tup & Testing	(0.03) x (DCC)	56,181	63,002	63,00	
(b) Mod		Estimated from Vendor Quote	included	included	include	
Total ICC:	,		805,262	903,031	903,03	
OTAL CAPITAL	. INVESTMENT (TCI):	DCC + ICC	2,677,964	3,003,103	3,003,10	
NDEOT OPER 1	TIMO COSTO (DOO): (-)					
(1) Operatin	TING COSTS (DOC): (a)					
		COO/hr: 4 hours par day: 1 460 hr/vr	32,120	32,120	32,12	
Operator		\$22/hr; 4 hours per day; 1,460 hr/yr	•			
Supervis		15% of operator cost	4,818	4,818	4,81	
(2) Maintena	ance (a)					
Labor		Equivalent to Operating Labor	36,938	36,938	36,93	
Materials	6	Equivalent to Maintenance Labor	36,938	36,938	36,93	
(3) Utilities (	b)	•				
	Injection System Electricity	\$34/MW-hr and 108 MW-hr /yr/ boiler	11,016	12,668	6,33	
	Electricity Icrease	Based on 4 inch pressure drop across system	17,385	17,385	8,69	
(U) Faii	Electricity icrease		17,000	17,000	0,00	
( ) 5 !! .!		for each boiler	4 405	4 000	75	
	on water (c)	1.2 gpm @ \$0.60/1000 gal raw	1,135	1,306	75	
(4) Chemica	ils and Materials (c)					
Urea bas	se chemical	120,000 gallon/yr for 80% @ \$1.00 / gal	360,000	414,000	207,00	
		for each boiler at 80% removal				
Catalyst	Replacement	Once per three years @ \$100,000 for 80%	100,000	125,000	78,12	
oalaiysi	nopiacomon.	for each boiler	100,000	.20,000	,	
Total DOC:			600 350	601 172	411,71	
TOTAL DOC:		(1) + (2) + (3) + (4)	600,350	681,173	411,71	
NDIRECT OPER	RATING COSTS (IOC): (a)					
(7) Overhea		60% of oper. labor & maintenance	66,488	66,488	66,48	
(0) Property	Tayon	19/ of total against invastment	26 790	30,031	30,03	
(8) Property		1% of total capital investment	26,780			
(9) Insuranc	ө	1% of total capital investment	26,780	30,031	30,03	
(10) Administ	ration	2% of total capital investment	53,559	60,062	60,06	
Total IOC:		(7) + (8) + (9) + (10)	173,607	186,613	186,61	
CAPITAL RECO	VERY COSTS (CRC):	CRF of 0.142 times TCI (10 yrs @ 7%)	380,271	426,441	426,44	
					·	
INNUALIZED C	OSTS (AC):	DOC + IOC + CRF	1,154,228	1,294,226	1,024,77	
JNCONTROLLE	D NOx EMISSIONS (TPY) :	Proposed Limit	310	310	15	
OTAL NOx REI	MOVED:	80% or 90%	248	279	14	

Notes:

Based on proposal provided by Engelhard, 9/22/98

- (a) Factors and cost estimates reflect OAQPS Cost Manual, Section 3.
  (b) Utility rates reflect actual 1998 rates for SCC
  (c) 90% removal costs reflect manufacturer's recommendation of a 15% increase above the 80% removal costs.



# Department of Environmental Protection

Jeb Bush Governor Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

David B. Struhs Secretary

September 22, 1999

### CERTIFIED MAIL - RETURN RECEIPT REQUESTED

Mr. John L. West, General Manager Stone Container Corporation Post Office Box 26998 Jacksonville, Florida 32226-6998

Re: DEP File No. 0310067-004-AC (PSD-FL-252) Recycled Fiber Facility, Increase in steam rate

Dear Mr. West:

The United States Fish and Wildlife Services raised the attached issue in regards to the above referenced project. Please respond to their concern as well as to our letters dated September 8 and September 10, 1999.

The Department will resume processing this application after receipt of the requested information. If you have any questions regarding this matter, please call Syed Arif, P.E. at (850) 921-9528.

Sincerely,

A. A. Linero, P.E. Administrator New Source Review Section

AAL/sa

### Enclosure

cc: Doug Neely, EPA

John Bunyak, NPS

C. Kirts, DEP-NED

B. Oven, DEP-OSC

J. Manning, RESD

D. Roberts, Esq., HGSS

J. Antista, General Counsel, Fl Game & Fresh Water Fish Commission

D. Russ, Esq., Dept. of Community Affairs

E. M. Barker, Esq., Slott & Barker

L. N. Curtin, Esq., Holland & Knight

G. K. Radlinski, Esq., City of Jacksonville

N. B. Barnard, Esq., St. Johns River Water Management District

R. Vandiver, General Counsel, Fl Public Service Commission

David Buff, Golder Associates Inc.

### NOTE

To:

Al Linero

From:

Ellen Porter, USFWS

Subject:

Stone Container Corp—PSD Applicability and BACT

Date:

September 9, 1999

Stone Container Corporation (SCC) is requesting a modification of its permit to allow greater utilization of its boilers 1-3 at its recycled fiber facility in Jacksonville, Florida. The increase boiler utilization is a result of the plant changing paper grades to produce more medium weight paper products. NO<sub>x</sub> emissions would be limited to the current permit limit of 310 TPY, but would increase from actual levels of 7 TPY.

### **PSD Applicability**

Although there is no mention of PSD in the information provided, this would appear to be a major modification because SCC is changing its method of operation (making more medium weight paper) and the result of that change is an increase in NO<sub>x</sub> emissions from 7 TPY to 310 TPY.

### Best Available Control Technology (BACT) Review

SCR was dismissed on the premise that it is not economically feasible for application to these package boilers. However, the cost analysis provided by SCC lacks documentation and contains several errors that tend to inflate costs:

- Structural support costs were included with Purchased equipment Costs.
- Indirect Capital Costs were based upon Total Direct Costs instead of Purchased Equipment Costs as recommended by the EPA OAQPS Control Cost Manual.
- An unjustified cost for Working Capital was included.
- The interest rate used to calculate the Capital recovery Factor should be 7% as recommended by the OAQPS Control Cost Manual.

Our cost analysis (enclosed) estimated costs of over \$4700 per ton of NO<sub>x</sub> removed.

### **Conclusions and Recommendations**

- PSD applies to these boilers due to increased emissions resulting from a change in the method of operation.
- SCR may be economically feasible. SCC should provide justification for its cost estimates.

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#### Golder Associates Inc.

6241 NW 23rd Street, Suite 500 Gainesville, FL 32653-1500 Telephone (352) 336-5600 Fax (352) 336-6603



September 22, 1999

9837525

Florida Department of Environmental Protection Bureau of Air Regulation 2600 Blair Stone Road Tallahassee, FL 32399-2400

RECEIVED

SEP 23 1999

Attention: Mr. A. A. Linero, P.E.

RE:

STONE CONTAINER CORPORATION - JACKSONVILLE

DEP FILE NO. 0310067-004-AC (PSD-FL-252)

RECYCLED FIBER FACILITY – INCREASE IN STEAM RATE

**BUREAU OF AIR REGULATION** 

Dear Mr. Linero:

Stone Container Corporation (SCC) has received the Department's letters dated September 8 and 10, 1999, regarding SCC's proposed steam rate increase for the three steam boilers located at the Jacksonville recycle fiber mill. Each of the Department's comments are addressed below, in the same order as they appear in the letter.

1. Selective non-catalytic reduction (SNCR) involves injection of ammonia or urea into the boiler flue gases while the flue gases are within a specific temperature window. This temperature window is from 1,600 to 1,900°F. As a result, the SNCR ammonia injection system must be located in the boiler. The temperature at the stack, approximately 330 to 350°F, is insufficient for the SNCR chemical reaction to take place.

SCR is similar to SNCR but involves a catalyst which lowers the reaction temperature window to 600 to 1,000°, depending upon the type of catalyst employed. however, these temperatures only exist within the boiler itself, and the temperature at the stack is insufficient. As a result, the SCR system must be located within the boiler, and not at the stack.

It is also noted that the three steam boilers have relatively long ducts, which run from the boiler to the common stack. The ducts come together at the stack, but prior to the stack, are completely separate. Therefore, it is not technically feasible to install a single SCR or SNCR system to accommodate all three package boilers at SCC.

In regards to Table 5-2 of the application, it is not known which boilers are low heat release rate boilers versus high heat release rate boilers. Low heat release rate boilers are able to achieve lower NO<sub>x</sub> emissions due to their larger furnace volume compared to higher heat release rate boilers. They also would have been required to meet an NSPS

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limit under Subpart Db of 0.1 lb/MMBtu. SCC's three package boilers are high heat release rate boilers, and therefore the NSPS limit is 0.2 lb/MMBtu.

Past  $NO_x$  continuous emissions monitoring (CEM) data for SCC's three package boilers have indicated actual average emissions of 0.05 lb/MMBtu (based on 1997 data). RATA data from 1998 showed that  $NO_x$  emissions ranged from 0.09 to 0.13 lb/MMBtu. So the CEM data has indicated that the boilers actually achieve a comparable  $NO_x$  emission rate to the boilers cited in the Department's letter. However, the  $NO_x$  data for SCC is very limited simply because Cedar Bay has been supplying the majority of SCC's steam needs. Another factor to consider is that SCC often times operates its boilers at reduced loads in order to meet steam needs.  $NO_x$  emissions may be higher at these lower loads, since combustion efficiency may be reduced. Also, the majority of actual operation to date has been on natural gas, and operating on oil could cause higher  $NO_x$  emissions. A third factor is that the boilers will be operated at somewhat higher heat input and steam rates, which may lead to slightly higher  $NO_x$  emissions.

Based on these considerations, SCC desires to retain the 0.2 lb/MMBtu limit. As SCC has proposed, this limit would actually be reduced to 0.175 lb/MMBtu at the maximum heat input rate to the boilers. The proposed  $NO_x$  emissions limit, in conjunction with operation and maintenance of the boilers and burners according to the manufacturer's specifications, will insure that actual  $NO_x$  emissions are maintained at the lowest achievable level.

### 2. The condition is acceptable with the following minor revisions:

"The facility is limited to 640,000 lb/hr total steam **consumption** (380,000 lb/hr imported from the CBCP and 260,000 lb/hr produced by SCC). When CBCP is not in operation or operating at reduced rates, SCC is permitted to produce up to 450,000 lb/hr steam and import up to 190,000 lb/hr from CBCP. This allows a maximum firing rate of 645 MMBtu/hr for all three package boilers when the CBCP facility is **shut**down or operating at reduced rates.

Regarding the City of Jacksonville's letter dated September 9, and provided via the Department's letter dated September 10, the following response is provided. In April 1998, RESD granted SCC permission to operate each of the three boilers up to 150,000 lb/hr steam during the May 1998 stack testing. During the testing, each boiler individually could operate up to 150,000 lb/hr steam, while the other two boilers were operated at or below the permitted rate of 125,000 lb/hr steam. The purpose of the testing was to support the current request to increase the permitted steam rate of each boiler to 150,000 lb/hr steam.

The May 8, 1998 compliance tests were performed at steam rates between 140,000 and 145,000 lb/hr steam. This is within the 90% of the maximum requested steam production rate of 150,000 lb/hr for each boiler. The heat input rates were between 172 and 187 MMBtu/hr, or between 80 to 87 percent of the requested maximum heat input of 215 MMBtu/hr. However, this merely indicates that the boiler was operating more efficiently than designed.

It is believed that reasonable assurance has been provided through the past CEM data and compliance test data that the proposed emission limit can be met. However, to provide further assurance that the proposed limit of 0.2 lb/MMBtu (0.175 lb/MMBtu at maximum heat input rate) can be met, SCC proposes to conduct additional stack testing on the boilers at the higher steam rate (up to 150,000 lb/hr steam). Cedar Bay is planning an outage during late October or early November of this year. SCC would like to obtain permission to operate the three boilers at up to 150,000 lb/hr steam each for up to four days when Cedar Bay is shutdown. During this testing, boiler operation would be adjusted and optimized (i.e., air flow, oxygen level, etc.) for optimum performance and emissions. SCC would invite RESD, and FDEP, to witness the testing. The testing will provide reasonable assurance that the emission limit can be met at the higher operating rates.

- 3 -

Thank you for consideration of these comments. Please call if you have any questions concerning this matter.

Sincerely,

G@LDER,ASSOCIATES INC.

DB/jkk

cc:

Joe Eskridge Terry Cole Buck Oven, FDEP-OSC J. Manning, RESD

\\GATORBAIT\DP\Projects\98\9837525a\01\#01ltr.dot

21 nent 970m on 701 bewelles is allowed for no more than 15

cc:

Addresses for

CERTIFICATE OF SERVICE

Stone Container

I DO HEREBY CERTIFY that a true and correct copy of the foregoing document has been sent by U.S. Mail to the following listed persons:

Doug Roberts, Esq.

Hopping Green Sams & Smith
P.O. Box 6526
Tallahassee, FL 32314

Gregory K. Radlinski, Esq.
City of Jacksonville
600 City Hall
220 E. Bay Street
Jacksonville, FL 32202

Terry Cole, Esq.
Scott Shirley, Esq.
Oertel Hoffman Fernandez & Cole
P.O. Box 6507
Tallahassee, FL 32314-6507

Nancy B. Barnard, Esq.
St. Johns River Water
Management District
P.O. Box 1429
Palatka, FL 32178-1429

Jim Antista, General Counsel
Florida Game & Fresh Water
Fish Commission
620 S. Meridian Road
Tallahassee, FL 32399-1600

Rob Vandiver, General Counsel
Bob Elias, Esquire
Bureau of Electric & Gas
Florida Public Service Comm.
2540 Shumard Oak Blvd..

David Russ, Esq.

Department of Community Affairs

2740 Centerview Dr.

Tallahassee, FL 32399-2100

James A. Heard, Esq. 1845 Lake Street No. 3 San Francisco, CA 94121

Earl M. Barker, Esq.

Slott & Barker

334 East Duval St.

Jacksonville, FL 32302

Lisa B. Cooper, Esq. Margol & Pennington 76 Laura St. Jacksonville, FL 32202

Note-there should be a sheet of labels w/ these addresses for easier

# Certificate of Service Page 2

Lawrence N. Curtin, Esq. Holland & Knight P.O. Drawer 810 Tallahassee, FL 32302

Charles W. Bostwick P.O. Box 12 Jacksonville, FL 32201-0012

this <u>25 2</u> day of July, 1996.

STATE OF FLORIDA DEPARTMENT OF ENVIRONMENTAL PROTECTION

CHARLES T. "CHIP" COLLETTE

Assistant General Counsel

3900 Commonwealth Blvd. MS 35 Tallahassee, FL 32399-3000 904/488-9730



# Department of Environmental Protection

Jeb Bush Governor Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

David B. Struhs Secretary

September 10, 1999

### CERTIFIED MAIL - RETURN RECEIPT REQUESTED

Mr. John L. West, General Manager Stone Container Corporation Post Office Box 26998 Jacksonville, Florida 32226-6998

Re: DEP File No. 0310067-004-AC (PSD-FL-252) Recycled Fiber Facility, Increase in steam rate

Dear Mr. West:

The Regulatory and Environmental Services Department of Jacksonville raised the attached incompleteness issue in regards to the above referenced project. Please respond to their concern as well as to the second incompleteness letter dated September 8, 1999 sent by the Department.

The Department will resume processing this application after receipt of the requested information. If you have any questions regarding this matter, please call Syed Arif, P.E. at (850) 921-9528.

Sincerely,

A. A. Linero, P.E. Administrator New Source Review Section

AAL/sa

#### Enclosure

cc: Doug Neely, EPA

John Bunyak, NPS

- C. Kirts, DEP-NED
- B. Oven, DEP-OSC
- J. Manning, RESD
- D. Roberts, Esq., HGSS
- J. Antista, General Counsel, Fl Game & Fresh Water Fish Commission
- D. Russ, Esq., Dept. of Community Affairs
- E. M. Barker, Esq., Slott & Barker
- L. N. Curtin, Esq., Holland & Knight
- G. K. Radlinski, Esq., City of Jacksonville
- N. B. Barnard, Esq., St. Johns River Water Management District
- R. Vandiver, General Counsel, Fl Public Service Commission

David Buff, Golder Associates Inc.

"Protect, Conserve and Manage Florida's Environment a

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### REGULATORY & ENVIRONMENTAL SERVICES DEPARTMENT

### Air and Water Quality Division

September 9, 1999



Mr. Syed Arif, Air Permit Engineer Florida Department of Environmental Protection Bureau of Air Regulation 2600 Blair Stone Road Tallahassee, FL 32399-2400

BUREAU OF AIR REGULATION

**RE:** Duval County – Air Pollution

Stone Container Corporation Permit Modification Request DEP File No. 031-0067-004-AC

Dear Mr. Arif:

The City of Jacksonville, Air and Water Quality Division (AWQD) has reviewed the referenced request dated August 11, 1999 and the stack test results on the three package boilers performed on May 8, 1998. The stack test results indicate the average actual heat input while firing natural gas during the tests on No. 1, No. 2, and No. 3 package boilers was 181 MMBtu/hr., 187 MMBtu/hr. and 172 MMBtu/hr. respectively. The steam production rate during the tests was between 140,000 and 145,000 lb/hr.

The referenced request is asking for an increase in the maximum heat input rate to 215 MMBtu/hr, an increase in steam production rate to 150,000 lb/hr. and to keep the existing allowable NO<sub>x</sub> emission rates of 0.2 lb/MMBtu, 34.94 lb/hr. and 153.1 tons/yr. per boiler. The AWQD believes Stone Container Corporation has not provided reasonable assurance that the three package boilers can demonstrate compliance with the NO<sub>x</sub> emission rates while operating at a heat input rate of 215 MMBtu/hr. The AWQD recommends Florida Department of Environmental Protection request Stone Container Corporation provide additional information providing reasonable assurance the existing allowable NO<sub>x</sub> emission rates can be achieved with a maximum heat input rate of 215 MMBtu/hr. while firing natural gas or No. 2 fuel oil.

Should you have any questions concerning this matter, please contact me at (904) 630-3484.

Very truly yours,

Richard L. Robinson, P.E., Manager Air Pollution Source Permitting Section

RLR/rt



# Department of Environmental Protection

Jeb Bush Governor Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

David B. Struhs Secretary

September 8, 1999

### CERTIFIED MAIL - RETURN RECEIPT REQUESTED

Mr. John L. West, General Manager Stone Container Corporation Post Office Box 26998 Jacksonville, Florida 32226-6998

Re: DEP File No. 0310067-004-AC (PSD-FL-252) Recycled Fiber Facility, Increase in steam rate

Dear Mr. West:

The Department has received the response to our initial incompleteness letter of August 4, 1998 on August 12, 1999, for an increase in the maximum permitted steam and heat input rate for Package Boilers Nos. 1-3 of the above referenced facility in Duval County. Based on our review of the response submitted, we have determined that additional information is needed in order to continue processing this application package. Please submit the information requested below pursuant to Rules 62-4.055 and 62-4.070(1), F.A.C.:

- 1. The response for the economic analysis for SCR and SNCR technologies included cost to install these technologies on all three package boilers. The application states that all three package boilers exhaust to a common stack. Please provide the economic analysis in \$/ton removed if a single SCR or SNCR system is installed in the common stack to reduce the NO<sub>x</sub> emissions. Additionally, explain why some of the facilities (Transamerican Refining Corporation, La; American Crystal Sugar Company, Mn; James River Corp; etc.) listed in Table 5-2 of the application employing the same controls of Low NO<sub>x</sub> burners and FGR are able to meet a much lower emission limit compared to the emission limit established for Stone Container.
- 2. During PSD permit amendment in 1995 (PSD-FL-198A), the following specific condition was removed and replaced by the current specific condition 4:
  - "The facility is limited to 640,000 lb/hr total steam production [380,000 lbs/hr imported from the Cedar Bay Cogeneration Project (CBCP) facility and 260,000 lbs/hr produced by Stone Container Corporation (SCC)]. When CBCP facility is not in operation or operating at reduced rates, SCC is permitted to make up the difference between the 380,000 lbs/hr imported steam rate and the steam production level that CBCP facility provides. This allows a maximum firing rate of 524 MMBtu/hr for all three package boilers when the CBCP facility is down."

Mr. John L. West September 8, 1999 Page 2 of 2

Please indicate if the following specific condition will be acceptable to SCC if PSD-FL-252 is issued:

"The facility is limited to 640,000 lb/hr total steam production [380,000 lb/hr imported from the CBCP and 260,000 lb/hr produced by SCC]. When CBCP facility is not in operation or operating at reduced rates, SCC is permitted to produce up to 450,000 lb/hr steam and import up to 190,000 lb/hr from CBCP. This allows a maximum firing rate of 645 MMBtu/hr for all three package boilers when the CBCP facility is down or operating at reduced rates."

If this condition is not acceptable, please provide reasons for the same.

The Department will resume processing this application after receipt of the requested information. If you have any questions regarding this matter, please call Syed Arif, P.E. at (850) 921-9528.

Sincerely,

A. A. Linero, P.E. Administrator New Source Review Section

### AAL/sa

### Enclosure

cc: Doug Neely, EPA

John Bunyak, NPS

- C. Kirts, DEP-NED
- B. Oven, DEP-OSC
- J. Manning, RESD
- D. Roberts, Esq., HGSS
- J. Antista, General Counsel, Fl Game & Fresh Water Fish Commission
- D. Russ, Esq., Dept. of Community Affairs
- E. M. Barker, Esq., Slott & Barker
- L. N. Curtin, Esq., Holland & Knight
- G. K. Radlinski, Esq., City of Jacksonville
- N. B. Barnard, Esq., St. Johns River Water Management District
- R. Vandiver, General Counsel, Fl Public Service Commission

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PS Form 3800, April 1995	DEP File No.0 (PSD-FL-252)	0310067-004-AC				

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the reverse side	SENDER:  Complete items 1 and/or 2 for additional services.  Complete items 3, 4a, and 4b.  Print your name and address on the reverse of this form so that we card to you.  Attach this form to the front of the mailpiece, or on the back if space permit.  Write "Return Receipt Requested" on the mailpiece below the article The Return Receipt will show to whom the article was delivered and delivered.	does not number.	I also wish to re following service extra fee):  1.	es (for an see's Address ed Delivery	eipt Service.
ADDRESS completed on	3. Article Addressed to:  Mr. John L. West, General Manager Stone Container Corporation Post Office Box 26998 Jacksonville, Florida 32226-6998	4b. Service  Registere  Express	618 137 Type ed Mail ceipt for Merchandise	CO	for using Return Rec
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8	PS Form <b>3811.</b> December 1994 102	595-98-B-0229	Domestic Ret	urn Receipt	

### Golder Associates Inc.

6241 NW 23rd Street, Suite 500 Gainesville, FL 32653-1500 Telephone (352) 336-5600 Fax (352) 336-6603

August 11, 1999

9837525

RECEIVED

AUG 16 1999

BUREAU OF AIR REGULATION

Florida Department of Environmental Regulation Safety & Coordination Office 2600 Blair Stone Road, MS 48 Tallahassee, FL 32399-2400

Attention: Mr. Buck Oven

RE: Stone Container Corporation - Jacksonville

Site Certification PA88-24A

Recycled Fiber Facility - Increase in Steam Rate

Dear Mr. Oven:

Stone Container Corporation (SCC) has requested modification of its current prevention of significant deterioration (PSD) permit to allow an increase in the maximum steam rate for the three steam boilers located at their Jacksonville recycle paper mill. This request was sent to the Bureau of Air Regulation in June 1998. The Department issued a request for additional information, and SCC has recently responded to this request. Therefore, the Department will now resume its review of the project.

SCC is requesting that the maximum steam rate for each package boiler be increased from 125,000 lb/hr to 150,000 lb/hr. The reason for this request is that SCC is changing the grades of paper it produces, and more steam is needed for the process. SCC will continue to rely on Cedar Bay for the majority of its steam needs.

Although SCC is increasing the maximum steam rates on the boilers, SCC is not requesting any change in its already permitted allowable  $NO_x$  emissions of 0.2 lb/MMBtu, 34.94 lb/hr per boiler, and 310 TPY total all three boilers. SCC is permitted for this level of emissions now, and these emissions have undergone full regulatory review in previous permitting. SCC is only requesting a change in the maximum hourly steam production rate from 125,000 lb/hr per boiler to 150,000 lb/hr per boiler.

It is emphasized that SCC has no intention of operating independent of Cedar Bay, as long as Cedar Bay continues to provide SCC steam on a reliable basis. Cedar Bay now has routine shutdowns for both planned and unplanned maintenance. However, catastrophic events have occurred at power plants in the past, which have shutdown such facilities for more than a year. Although such an event at Cedar Bay is very unlikely, it is not impossible.

SCC has customers to which it is contractually obligated to supply paper. If SCC cannot produce paper for whatever reason, SCC will lose its customers. Therefore a steam shortage

is not an option. SCC cannot be in a position where a long-term shutdown at Cedar Bay occurs, and SCC is not permitted to generate the necessary steam to operate. As a result, SCC must be permitted for full operation.

The Site Certification (PA88-24A) Conditions of Certification (COC) for Cedar Bay Cogeneration Project will require modification. However, the only condition requiring modification is that related to SCC steam boiler emissions (Condition II.E.), and that only so far as the limitation on steam rate for the SCC boilers (i.e., 375,000 lb/hr steam to be revised to 450,000 lb/hr steam). No change in emission limits contained in the COC is necessary or requested.

As described previously, it is imperative that SCC obtain this approval by October 25, 1999 in order to avoid curtailment of production.

Attached is the modification fee of \$10,000. Thank you for review of this information. Please call if you have any questions concerning this matter.

Sincerely,

GOLDER ASSOCIATES INC.

Downiel a Buff

David A. Buff, P.E. Principal Engineer

Florida P.E. #19011

SEAL

DB/jkk

**Enclosures** 

cc: Joe Eskridge

Terry Coie

A. A. Linero

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#### **Stone Container Corporation**

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Stone Container Corporation

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401 ALTON STREET, P.O. BOX 276 ALTON, IL 62002-2276

CHASE MANHATTAN BANK DELAWARE 1201 Market Street Wilmington, DE 19801

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amount \$10,000.00

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THIS CHECK NOT VALID UNLESS PRESENTED FOR

PAY to the order of

FL. DEPART OF ENVIRONPROTECT OFFICE OF SITING COORDINATION 2600 BLAIRE STONE ROAD, MS48 TALLAHASSE

2nd SIGNATURE REQUIRED IF OVER \$5,000. Stone Container Corporation

PAYMENT WITHIN 180 DAYS FROM DATE OF ISSUE

#### Golder Associates Inc.

6241 NW 23rd Street, Suite 500 Gainesville, FL 32653-1500 Telephone (352) 336-5600 Fax (352) 336-6603



August 11, 1999

9837525

Florida Department of Environmental Protection Bureau of Air Regulation 2600 Blair Stone Road Tallahassee, FL 32399-2400 RECEIVED

AUG 12 1999

**BUREAU OF AIR REGULATION** 

Attention: Mr. A. A. Linero, P.E.

RE: Stone Container Corporation - Jacksonville

DEP File No. 0310067-004-AC (PSD-FL-252) Recycled Fiber Facility – Increase in Steam Rate

Dear Mr. Linero:

Stone Container Corporation (SCC) has received the Department's letter dated August 4, 1998, and is now ready to move forward with obtaining approval for the steam rate increase. SCC would like to obtain approval for this request no later than October 25, 1999. On this date, Cedar Bay will begin an outage. If SCC cannot operate their boilers at the increased steam rate, they will be forced to cut production during this outage.

Each of the Department's comments is addressed below, in the same order as they appear in the letter.

- 1. A request to modify the Conditions of Certification (COC) for the Cedar Bay Cogeneration Project (PA88-24A) is being submitted concurrently with this request to modify the air construction permit. A copy of the submittal is will be forthcoming to you.
- 2. Past operation of the three steam boilers has typically been as standby in the event that Cedar Bay loses steam production. As such. SCC normally keeps one boiler on idle in case of a loss in steam by Cedar Bay; SCC can immediately replace the steam loss and avoid an interruption in production. So normally, one boiler is always operating, but at a very low load. On a very infrequent basis, Cedar Bay is shutdown and during these times SCC must generate its own steam. During 1997 and 1998, total steam production from all three boilers averaged approximately 319,800,100 lbs steam per year. This is equivalent to one boiler operating approximately 2,560 hr/yr at full load.

The NO<sub>x</sub> emissions are based on continuous emission monitoring (CEM) data, not stack test data. The requested allowable of 310 tons per year (TPY) is the current permitted emissions for the three boilers combined. SCC is only asking to retain the current permitted level, in terms of both lb/hr and TPY, even though the

maximum hourly steam rate will increase. Thus, at maximum load of 150,000 lb/hr steam (215 MMBtu/hr), the maximum hourly  $NO_x$  emission rate for each boiler of 34.94 lb/hr (0.2 lb/MMBtu) will equate to an  $NO_x$  emission rate of 0.175 lb/MMBtu. It is noted that SCC has already accepted an annual limit (310 TPY) that is considerably lower than the maximum each boiler could emit. At maximum year-around operation, each boiler could emit 153.1 TPY, which equates to 459.3 TPY total for all three boilers.

SCC is requesting to retain the current 310 TPY  $NO_x$  emission rate in the event that Cedar Bay is unable to supply SCC with the necessary steam to meet production. SCC is in the process of changing paper grades and plans on producing more medium weight paper products. These changes will require up to 450,000 lb/hr steam because of the heavier weight of the paper. The ability to operate at the higher steam rate, and to operate at any time Cedar Bay is shut down, is required in order to insure production needs are met. In summary, SCC must retain the flexibility to operate all its boilers on a year-around basis, although this is unlikely to actually occur.

In this regard, SCC would like to clarify the language presented in Attachment A, page 1-1, of the June 1998 PSD permit application. SCC has not intention of operating independently of Cedar Bay. However, it is prudent for SCC to retain the ability to operate in the event that Cedar Bay does not operate, for whatever reason or length of shutdown. Cedar Bay now experiences both planned and unplanned shutdowns for maintenance and other reasons. Catastrophic events have occurred at power plants in the past, which have shut down such facilities for more than a year.

As requested, an economic analysis for add-on NO<sub>x</sub> control technologies was 3. performed. Both selective catalytic reduction (SCR) and selective non-catalytic reduction (SNCR) technologies were evaluated. The results of the economic analysis are presented in Tables 1 and 2. For SCR (Table 1), the estimated capital cost to install SCR on all three boilers is \$3.36 million (for the 90% NOx removal case). Assuming 100% capacity factor operation, the total annual operating cost is estimated at \$1.43 million. The resulting cost effectiveness is \$5,100/ton of NO<sub>x</sub> removed. However, as described above, actual operation is expected to be well below 100% capacity factor. If it is conservatively assumed that 50% capacity operation is achieved in the future, then the total annual operating cost becomes \$1.15 million, and the cost effectiveness then becomes \$8,300/ton of NO<sub>x</sub> removed. As presented in the application, actual NO<sub>x</sub> emissions have only been 7 TPY. If this actual historic operation were used for cost effectiveness calculations, the cost effectiveness would become (assuming no direct operating costs) approximately \$120,000/ton of NO, removed. The cost effectiveness of SNCR is much higher than SCR due to the lower removal efficiency expected for SNCR (refer to Table 2).

Based on the above analysis, the application of SCR or SNCR to the existing SCC boilers is economically infeasible. A review of the BACT Clearinghouse information reveals that no boilers in the size range of the SCC boilers (i.e., 100-300

CC: (continued:

J. n. Curtin, H4K y. Radlinski, City of Jax NB Barrard SJRWMD R. Vandiver, PSC

Syld Arif, BAR, DEP

MMBtu/hr) which fire primarily natural gas have been required to install SCR or SNCR as BACT. All have employed low-  $NO_x$  burners and flue gas recirculation (FGR), which the SCC boilers employ. This is a result of the low  $NO_x$  emissions achieved by boilers, which utilize low-  $NO_x$  burners and FGR.

- 4. The requested documentation is attached.
- 5. A response to the Department of Community Affairs letter is attached. This response is being sent directly to the DCA.

As described previously, it is imperative that SCC obtain this approval by October 25, 1999 in order to avoid curtailment of production.

Thank you for consideration of these comments. Please call if you have any questions concerning this matter.

Sincerely,

GOLDER ASSOCIATES INC.

David A. Buff, P.E.

Frincipal Engineer

Florida R.E. #19011

SEA1

**Enclosures** 

Mind BKk

cc: Joe Eskridge Terry Cole

G:\DATA\DP\PROJECTS\98\9837\9837525A\07\07-ltr.doc

NED D. Oven Duval Co. D. Roberts, HGS+S Q. Antista, Her. Coun. FG+F D. Russ, Esq., Dept. of C.A. E. M. Barker, Esq. 5+B

	Table 1. Cost Effectiveness for Using SCR to Control NOx Emissions for Boiler Nos.1-3, Stone Container Corp.  Maximum Operation  50% Operation				
Cost Home	Ocal Fasters	80%	90% Pomoval	90%	
Cost Items	Cost Factors	Removal (1998 \$)	Removal (1998 \$)	Removal (1998 \$)	
RECT CAPITAL COSTS (DCC):		(1000 4)	(1000 \$)	(1000 4)	
(1) Purchased Equipment Cost					
(a) Basic Equipment/Services	Based on Vendor Quote (c)	1,050,000	1,200,000	1,200,000	
(b) Instrumentation	0.10 x 1a	105,000	120,000	120,000	
(c) Ammonia Storage Tank	\$140 per 1000 lb mass flow	84,000	84,000		
(d) Additional Ductwork	Based on OAQPS Cost Control Manual, Ch. 1	120,000	120,000		
(f) Structural Support (a)	0.10 x (1a1e)	135,900	152,400	152,400	
(g) Freight	0.05 x 1a	included	included	included	
(h) Sales Tax (Florida)	0.06 x (1a1f)	89,694	100,584	100,58	
(i) Subtotal	(1a1h)	1,584,594	1,776,984	1,776,98	
(2) Direct Installation (a)	0.30 x (1)	475,378	533,095	533,09	
Total DCC:	(1i) + (2)	2,059,972	2,310,079	2,310,079	
Total Book.	(11) + (2)	2,000,012	2,510,075	2,510,07	
IDIRECT CAPITAL COSTS (ICC): (a) (3) Indirect Installation Costs					
(a) Technology License Fee	Provided from Vendor Quote	included	included	include	
	•	included	included	include	
(b) Engineering & Supervision	Provided from Vendor Quote				
(c) Construction & Field Expenses	(0.05) x (DCC)	102,999	115,504	115,50	
(d) Construction Contractor Fee	(0.10) x (DCC)	205,997	231,008	231,00	
(e) Contingencies	(0.25) x (DCC) - based on retrofit	514,993	577,520	577,520	
(4) Other Indirect Costs					
(a) Startup & Testing (a)	(0.03) x (DCC)	61,799	69,302	69,30	
(b) Model Study	Estimated from Vendor Quote	included	included	include	
(c) Working Capital	30-day DOC	50,029	56,764	34,310	
Total ICC:	(3) + (4)	935,817	1,050,098	1,027,64	
Total ICC.	(3) + (4)	333,017	1,050,050	1,027,04	
OTAL CAPITAL INVESTMENT (TCI):	DCC + ICC	2,995,789	3,360,178	3,337,72	
RECT OPERATING COSTS (DOC):					
(1) Operating Labor					
Operator	\$22/hr; 4 hours per day; 1,460 hr/yr	32,120	32,120	32,12	
Supervisor	15% of operator cost	4,818	4,818	4,81	
(2) Maintenance (a)			·		
Labor	Equivalent to Operating Labor	36,938	36,938	36,93	
Materials		36,938	36,938		
	Equivalent to Maintenance Labor	30,330	30,330	30,33	
(3) Utilities (b)	#2 4/4 # A L	11.016	12,668	6,33	
(a) Urea Injection System Electricity	\$34/MW-hr and 108 MW-hr /yr/ boiler	11,016	•		
(b) Fan Electricity Icrease	Based on 4 inch pressure drop across system	17,385	17,385	8,69	
	for each boiler				
(c) Dilution water (c)	1.2 gpm @ \$0.60/1000 gal raw	1,135	1,306	75	
(4) Chemicals and Materials (c)					
Urea base chemical	120,000 gallon/yr for 80% @ \$1.00 / gal	360,000	414,000	207,00	
Outstand David and and	for each boiler at 80% removal	400.000	. 405.000	70.40	
Catalyst Replacement	Once per three years @ \$100,000 for 80%	100,000	125,000	78,12	
	for each boiler			= 4	
Total DOC:	(1) + (2) + (3) + (4)	600,350	681,173	411,71	
IDIRECT OPERATING COSTS (IOC): (a)					
(7) Overhead	60% of oper, labor & maintenance	66,488	66,488	66,48	
(7) Overnead	oo w or oper, labor a maintenance	00,400	00,400	00,10	
(8) Property Taxes	1% of total capital investment	29,958	33,602	33,37	
(9) Insurance	1% of total capital investment	29,958	33,602	33,37	
(10) Administration	2% of total capital investment	59,916	67,204	66,75	
• •	•				
Total IOC:	(7) + (8) + (9) + (10)	186,320	200,896	199,99	
APITAL RECOVERY COSTS (CRC):	CRF of 0.1627 times TCI (10 yrs @ 10%)	487,415	546,701	543,04	
	DOC + IOC + CRF	1,274,085	1,428,769	1,154,76	
NNUALIZED COSTS (AC):	DOC + IOO + ORF	1,274,000	1,420,709	1,134,70	
INCONTROLLED NOX EMISSIONS (TPY) :	Proposed Limit	310	310	15	
OTAL NOx REMOVED:	80% or 90%	248	279	14	
	\$ per ton of NOx Removed	5,137	5,121	8,27	
COST EFFECTIVENESS:					

Notes:

Based on proposal provided by Engelhard, 9/22/98

<sup>(</sup>a) Factors and cost estimates reflect OAQPS Cost Manual, Section 3.
(b) Utility rates reflect actual 1998 rates for SCC

<sup>(</sup>c) 90% removal costs reflect manufacturer's recommendation of a 15% increase above the 80% removal costs.

	trol NOx Emissions for Package Boiler Nos.1-3, S	Maximu m	50% Operation		
		50%			
Cost items	Cost Factors	removal (d)	to	Adjusted to	
	33011 430073	(1995 dollars)	1997 dollars (e)	1997 dollars (e)	
DIRECT CAPITAL COSTS (DCC):		(1000 donais)	1007 dollars (c)	roor donars (c)	
(1) Purchased Equipment Cost					
(a) Basic Equipment/Services	Based on Vendor Quote	1,158,720	1,175,632	1,175,632	
(b) Reductant Tank & Auxiliary System	included	included	included	included	
(c) Instrumentation & Controls (a)		115,872	117,563	117,563	
(d) Structural Support	0.10 x (1a1b)	115,872	117,563	117,563	
(e) Freight	0.10 x (1a1b)	69,523	70,538	70,538	
(f) Sales Tax (Florida)	0.05 x (1a1d)	83,428	84,645	84.645	
	0.06 x (1a1d) (1a1f)	1,543,415	1,565,941	1,565,941	
(g) Subtotal	(1a1) Based on Vendor Quote	288,000			
(2) Direct Installation (a)			292,203	292,203	
Total DCC:	(1g) + (2)	1,831,415	1,858,145	1,858,145	
NDIRECT CAPITAL COSTS (ICC): (a)				-	
(3) Indirect Installation Costs	55 414 34 4 6 4	to disassa	Paralla da d	:	
(a) Technology License Fee	Estimated from Vendor Quote	included	included	included	
(b) Engineering & Supervision (a)	(0.20) x (DCC)	366,283	371,629	371,629	
(c) Construction & Field Expenses (a)	(0.20) x (DCC)	366,283	371,629	371,629	
(d) Construction Contractor Fee (a)	(0.10) x (DCC)	183,142	185,814	185,814	
(e) Contingencies	(0.25) x (DCC)	457,854	464,536	464,536	
(4) Other Indirect Costs					
(a) Startup & Testing (a)	Estimated from Vendor Quote	included	included	included	
(b) Model Study	Estimated from Vendor Quote	N/A	N/A	N/A	
(c) Working Capital	30-day DOC	46,403	46,403	27,819	
Total ICC:	(3) + (4)	1,419,964	1,440,011	1,421,427	
TOTAL CAPITAL INVESTMENT (TCI):	DCC + ICC	3,251,379	3,298,156	3,279,572	
DIDECT OPERATING COSTS (DOC):					
DIRECT OPERATING COSTS (DOC):					
(1) Operating Labor	600/h 4 h - 1 l 4 400 h - 1 -	22.420	22.420	32.120	
Operator	\$22/hr; 4 hr/day; 1,460 hr/yr	32,120	32,120		
Supervisor (a)	15% of operator cost	4,818	4,818	4,818	
(2) Maintenance (a)					
Labor	Equivalent to Operating Labor	36,938	36,938	36,938	
Maintenance	Equivalent to Maintenance Labor	36,938	36,938	36,938	
(3) Utilities (b)					
(a) Urea Injection System Electricity	\$34/MW-hr and 70 MW-hr /yr/boiler	7,140	7,140	3,570	
(b) Dilution water (c)	4.1 gpm @ \$0.60/1000 gal/boiler	3,879	3,879	1,939	
(4) Chemicals and Materials (c)					
Reductant	145,000 gallon/yr @ \$1.00 / gal	435,000	435,000	217,500	
	for each boiler	·	•		
Total DOC:	(1) + (2) + (3) + (4)	556,833	556,833	333,823	
NDIRECT OPERATING COSTS (IOC): (a)					
(7) Overhead (a)	60% of oper, labor & maintenance	22,163	22,163	22,163	
(8) Property Taxes (a)	1% of total capital investment	32,514	32,982	32,796	
	1% of total capital investment	32,514	32,982	32,796	
(9) Insurance (a)			-	65,591	
(10) Administration (a)	2% of total capital investment	65,028	65,963		
Total IOC:	(7) + (8) + (9) + (10)	152,218	154,089	153,346	
CAPITAL RECOVERY COSTS (CRC):	CRF of 0.1627 times TCI (10 yrs @ 10%)	528,999	536,610	533,586	
ANNUALIZED COSTS (AC):	DOC + IOC + CRF	1,238,050	1,247,532	1,020,756	
UNCONTROLLED NOx EMISSIONS (TPY) :	Proposed Limit	310	310	155	
TOTAL NOx REMOVED:	50%	155	155	78	
TOTAL NOX REMOVED.	•••				

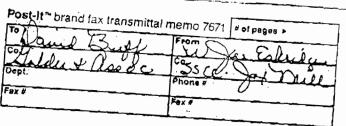
<sup>(</sup>a) Factors and cost estimates reflect OAQPS Cost Manual.
(b) Utility rates reflect actual 1998 rates for SCC.

<sup>(</sup>c) Uncontrolled emissions reflect proposed limit
(d) Cost estimates based on 1995 dollars - first quarter (vendor quote April 1995).
(e) Cost estimates adjusted to third quarter 1997 dollars using the EPA's, Escalation Indexes for Air Pollution Control Costs.

REGULATORY & I

Air and Water Qua

April 27, 1998





Mr. W. Joe Eskridge Environmental Engineer Stone Container Corporation Post Office Box 26998 Jacksonville, Florida 32218

RE: Request For Increased Process Rate During Compliance Testing

No. 1 - No. 3 Package Steam Boilers Permit Number: AO16-262702

Stone Container Corporation (SCC) Correspondence of April 16, 1998

Dear Mr. Eskridge:

This is to acknowledge receipt of the above captioned Stone Container Corporation (SCC) correspondence, submitted April 20, 1998.

The Air and Water Quality Division (AWQD) hereby grants SCC permission to operate each of the three (3) emission units at a steam production rate not to exceed 150,000 lbs/hr. during the upcoming May, 1998 stack testing series. As stated in SCC's correspondence, the increased steam production rate is only permissible for the individual boilers when tested; the other two (2) boilers shall be operated at a steam production rate at or below the permitted 125,000 lbs/hr.

If there are any questions concerning this matter, please contact Mr. Wayne Walker at (904) 630-3484.

Very truly yours,

Wayne E. Tutt, QEP Associate Engineer

WET/WLW/rt

c: Ms. Rita Smith, Engineer, DEP Mr. Richard Robinson, P.E., AWQD AQD File 2155 B (0067)



# Stone Container Corporation

Containerboard and Paper Division

P.O. Box 26998 Jacksonville, Florida 32226-6998

904-751-6400

April 16, 1998

Rita Felton-Smith Engineer Florida Department of Environmental Protection 7825 Baymeadows Way Suite B-200 Jacksonville, Florida 32256-7590

Wayne Walker,
Regulatory and Environmental
Services Division
Air and Water Quality Division
City Hall - St. James Building
117 West Duval Street - Suite 225
Jacksonville, Florida 32202

Dear Ms. Felton-Smith, Mr. Walker;

We will be performing our annual stack testing (RATA) on May 7 - 9, 1998.

We request permission to run each boiler at 150,000 lbs/hr of steam production for the duration of the test on that particular boiler. The other two (2) boilers will be run at a lower rate.

The purpose of this testing at higher rate is to generate data to support our construction permit request to fire the boilers at 150,000 lbs/hr rate.

Sincerely

STONE CONTAINER CORPORATION Jacksonville Mill

W. Joe Eskridge.

Environmental Engineer

/maa

#### Golder Associates Inc.

6241 NW 23rd Street, Suite 500 Gainesville, FL 32653-1500 Telephone (352) 336-5600 Fax (352) 336-6603



August 11, 1999

9837525

Department of Community Affairs Bureau of State Planning 2555 Shumard Oak Boulevard Tallahassee, FL 32399-2100

Attention: Mr. James L. Quinn

RE: Stone Container Corporation - Jacksonville DEP File No. 0310067-004-AC (PSD-FL-252)

Recycled Fiber Facility - Increase in Steam Rate

Dear Mr. Quinn:

Stone Container Corporation (SCC) has received the Department of Community Affairs (DCA) letter dated August 4, 1998, and is providing this letter for response and clarification of SCC's reasons for requesting an increase in steam production. First, it is emphasized that SCC is not requesting any change in its already permitted allowable NO<sub>x</sub> emissions of 0.2 lb/MMBtu, 34.94 lb/hr per boiler, and 310 TPY total all three boilers. SCC is permitted for this level of emissions now, and these emissions have undergone full regulatory review in previous permitting. SCC is only requesting a change in the maximum hourly steam production rate from 125,000 lb/hr per boiler to 150,000 lb/hr per boiler. The reason for this change is that SCC is changing the grades of paper it produces, and more steam is needed for the process.

SCC has no intention of operating independently of Cedar Bay, as long as Cedar Bay continues to provide SCC steam on a reliable basis. Cedar Bay now has routine shutdowns for both planned and unplanned maintenance. However, catastrophic events have occurred at power plants in the past, which have shut down such facilities for more than a year.

SCC has customers to which it is contractually obligated to sell paper. If SCC cannot produce paper for whatever reason, SCC will lose its customers. Therefore a steam shortage is not an option. SCC cannot be in a position where a long-term shutdown at Cedar Bay occurs, and SCC is not permitted to generate the necessary steam to operate. As a result, SCC must be permitted for full operation. Future actual operation is expected to result in the equivalent of one boiler operating at full load year-around.

The Site Certification (PA88-24A) Conditions of Certification (COC) for Cedar Bay Cogeneration Project will require modification. However, the only condition requiring modification is that related to SCC steam boiler emissions (Condition II.E.), and that only in

so far as the limitation on steam rate for the SCC boilers (i.e., 375,000 lb/hr steam to be revised to 450,000 lb/hr steam). No change in emission limits contained in the COC is necessary or requested.

The SCC mill over the last few years has converted from a paper mill to a 100% recycle mill. This has resulted in major decreases in emissions to the atmosphere and discharges to water. It also resulted in almost total elimination odors.

As described previously, it is imperative that SCC obtain this approval by October 25, 1999 in order to avoid curtailment of production.

Thank you for review of this information. Please call if you have any questions concerning this matter.

Sincerely,

GOLDER ASSOCIATES INC.

David A. Buff, P.E. Principal Engineer Florida P.E. #19011

SEAL

DB/jkk

Enclosures

cc: Joe Eskridge Terry Cole

A. A. Linero

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#### Golder Associates Inc.

6241 NW 23rd Street, Suite 500 Gainesville, FL 32653-1500 Telephone (352) 336-5600 Fax (352) 336-6603



August 11, 1999

9837525

Florida Department of Environmental Regulation Safety & Coordination Office 2600 Blair Stone Road, MS 48 Tallahassee, FL 32399-2400

Attention: Mr. Buck Oven

RE: Stone Container Corporation - Jacksonville

Site Certification PA88-24A

Recycled Fiber Facility - Increase in Steam Rate

Dear Mr. Oven:

Stone Container Corporation (SCC) has requested modification of its current prevention of significant deterioration (PSD) permit to allow an increase in the maximum steam rate for the three steam boilers located at their Jacksonville recycle paper mill. This request was sent to the Bureau of Air Regulation in June 1998. The Department issued a request for additional information, and SCC has recently responded to this request. Therefore, the Department will now resume its review of the project.

SCC is requesting that the maximum steam rate for each package boiler be increased from 125,000 lb/hr to 150,000 lb/hr. The reason for this request is that SCC is changing the grades of paper it produces, and more steam is needed for the process. SCC will continue to rely on Cedar Bay for the majority of its steam needs.

Although SCC is increasing the maximum steam rates on the boilers, SCC is not requesting any change in its already permitted allowable  $NO_x$  emissions of 0.2 lb/MMBtu, 34.94 lb/hr per boiler, and 310 TPY total all three boilers. SCC is permitted for this level of emissions now, and these emissions have undergone full regulatory review in previous permitting. SCC is only requesting a change in the maximum hourly steam production rate from 125,000 lb/hr per boiler to 150,000 lb/hr per boiler.

It is emphasized that SCC has no intention of operating independent of Cedar Bay, as long as Cedar Bay continues to provide SCC steam on a reliable basis. Cedar Bay now has routine shutdowns for both planned and unplanned maintenance. However, catastrophic events have occurred at power plants in the past, which have shutdown such facilities for more than a year. Although such an event at Cedar Bay is very unlikely, it is not impossible.

SCC has customers to which it is contractually obligated to supply paper. If SCC cannot produce paper for whatever reason, SCC will lose its customers. Therefore a steam shortage

August 11, 1999 Project No. 9837525

is not an option. SCC cannot be in a position where a long-term shutdown at Cedar Bay occurs, and SCC is not permitted to generate the necessary steam to operate. As a result, SCC must be permitted for full operation.

The Site Certification (PA88-24A) Conditions of Certification (COC) for Cedar Bay Cogeneration Project will require modification. However, the only condition requiring modification is that related to SCC steam boiler emissions (Condition II.E.), and that only so far as the limitation on steam rate for the SCC boilers (i.e., 375,000 lb/hr steam to be revised to 450,000 lb/hr steam). No change in emission limits contained in the COC is necessary or requested.

As described previously, it is imperative that SCC obtain this approval by October 25, 1999 in order to avoid curtailment of production.

Attached is the modification fee of \$10,000. Thank you for review of this information. Please call if you have any questions concerning this matter.

Sincerely,

GOLDER ASSOCIATES INC.

David A. Buff, P.E. Principal Engineer Florida P.E. #19011

SEAL

DB/jkk

**Enclosures** 

cc: Joe Eskridge

Terry Cole
A. A. Linero

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# Department of Environmental Protection

Lawton Chiles Governor Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Virginia B. Wetherell Secretary

August 4, 1998

### CERTIFIED MAIL - RETURN RECEIPT REQUESTED

Mr. John L. West, General Manager Stone Container Corporation Post Office Box 26998 Jacksonville, Florida 32226-6998

Re: DEP File No. 0310067-004-AC (PSD-FL-252) Recycled Fiber Facility, Increase in steam rate

Dear Mr. West:

The Department has received the application on July 6, 1998 for an increase in the maximum permitted steam and heat input rate for Package Boilers Nos. 1-3 of the above referenced facility in Duval County. Based on our initial review of the proposed project, we have determined that additional information is needed in order to continue processing this application package. Please submit the information requested below to the Department's Bureau of Air Regulation:

- 1. Submit an additional \$10,000 to modify Conditions of Certification for Cedar Bay Cogeneration Project PA 88-24. The additional permitting fees should be sent to the Office of Siting Coordination. The modification request should address the removal of the key restriction placed in Condition of Certification No. II.E.1 regarding the maximum steam rate allowed for Stone Container. This request should be addressed to Buck Oven of the Office of Siting Coordination.
- 2. Table 3-3 of the application indicates the current actual emissions for NO<sub>x</sub> to be less than 7 tons per year. What was the steam rate production at this level of NO<sub>x</sub> emissions? How many stack tests were considered in determining the actual NO<sub>x</sub> emissions? What are the reasons for asking an enormously high allowable emission rate for NO<sub>x</sub> (310 TPY) when the actual emissions are down in single digit.
- 3. An economic analyses is required for various control technologies suggested in the BACT analyses. Please provide this information for SCR and SNCR control systems.
- 4. Provide the documentation that allowed Stone Container to conduct continuous NO<sub>x</sub> emission monitor relative accuracy testing at the proposed increased steam rate of 150,000 lb/hr.
- 5. Attached is a letter from the Department of Community Affairs. We invite your comments regarding this letter.

Mr. John L. West August 4, 1998 Page 2 of 2

We have not yet received comments from the U.S. Fish and Wildlife Service or from the EPA. Their comments will be forwarded to you as soon as we receive them.

The Department will resume processing this application after receipt of the requested information. If you have any questions regarding this matter, please call Syed Arif, P.E. at (850) 921-9528.

Sincerely,

A. A. Linero, P.E. Administrator

New Source Review Section

### AAL/sa

### Enclosure

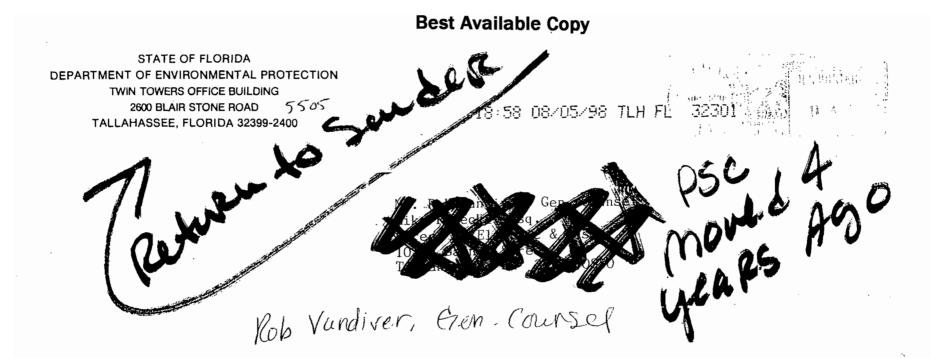
cc: Doug Neely, EPA

John Bunyak, NPS

- C. Kirts, DEP-NED
- B. Oven, DEP-OSC
- J. Manning, RESD
- -D. Roberts, Esq., HGSS
- J. Antista, General Counsel, Fl Game & Fresh Water Fish Commission
- D. Russ, Esq., Dept. of Community Affairs
- E. M. Barker, Esq., Slott & Barker
- L. N. Curtin, Esq., Holland & Knight
- K. Radlinski, Esq., City of Jacksonville
- N. B. Barnard, Esq., St. Johns River Water Management District
- R. Vandiver, General Counsel, Fl Public Service Commission
- L. B. Cooper, Esq., Margol & Pennington

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PS Form <b>3800</b> , April 1995	0310067-004	Ac				
PS	PSD-F1-25	52				

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on the reverse side?	■ Complete items 1 and/or 2 for additional services.  ■ Complete items 3, 4a, and 4b.  ■ Print your name and address on the reverse of this form so that we card to you.  ■ Attach this form to the front of the mailpiece, or ch the back if space permit.  ■ Write "Return Receipt Requested" on the mailpiece below the article ■ The Return Receipt will show to whom the article was delivered and delivered.	I also wish to receive the following services (for an extra fee):  1.  Addressee's Address 2.  Restricted Delivery Consult postmaster for fee.		
completed	3. Article Addressed to: Wist, Gen. 115r. Mr. John J. Wist, Jen. 115r. Stone Container Corp	4a. Article No.	25 659 401	
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s your <u>P</u>	6. Signature: (Addressee or Agent)  X	)		
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DEPARTMENT OF ELORIDA SASSON S

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STATE OF FLORIDA

# DEPARTMENT OF COMMUNITY AFFAIRS

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LAWTON CHILES
Governor

JAMES F. MURLEY Secretary

31 July 1998

A A. Linero
Administrator, New Source Review
Department of Environmental Protection
Twin Towers Office Building
2600 Blair Stone Road
Tallahassee, Florida 32399-2400

RECEIVED

. AUG 0.4 1998

BUREAU OF AIR REGULATION

Dear Mr. Linero:

RE: Stone Container Corporation's application for a modification to their PSD permit

Thank you for informing us of the Stone Container Corporation (SCC) application for modification of its current Prevention of Significant Deterioration (PSD) permit. We have reviewed the excerpts from SCC's application which were attached to your letter of 15 July 1998.

SCC is currently operating a recycled fiber paper mill in Jacksonville, Florida, adjacent to the Cedar Bay cogeneration facility. The Cedar Bay facility burns coal to produce steam which is then used to generate electrical power. As a cogenerator, some of the steam is used for another purpose. In this case, it is sent next door to the SCC plant for use in the paper-making process. According to SCC, its paper plant required additional steam beyond the amount supplied by Cedar Bay and therefore three package boilers were installed at the paper plant to supply the additional steam. SCC obtained a PSD permit for these boilers in 1993. This permit was amended in 1995 to allow increased steam production from the three boilers (125,000 lbs/hr steam for each of the boilers).

Now SCC is seeking to amend the PSD permit again to allow each boiler to produce 150,000 lbs/hr steam. The attached PSD report states that "Although at present SCC anticipates that this increased level of steam production will be needed infrequently, such as during a scheduled outage by Cedar Bay, SCC would like to plan for the future independently of Cedar Bay."

Though the Department does not object to SCC's understandable desire to continue operating its paper plant during those periods when the Cedar Bay power plant is offline for a scheduled outage, SCC's stated intention to plan for the future independently of Cedar Bay appears to go further than this. It suggests a future scenario in which SCC would be burning fossil fuel to

2555 SHUMARD OAK BOULEVARD • TALLAHASSEE, FLORIDA 32399-2100 Phone: 850.488.8466/Suncom 278.8466 FAX: 850.921.0781/Suncom 291.0781 Internet address: http://www.state.fl.us/comaff/dca.html A.A. Linero 31 July 1998 Page 2

produce all of the steam it needs in the paper-making process—all of the time. Cedar Bay would also be burning fossil fuel to produce steam, but only for generation of electrical power—it would not be supplying steam to the SCC plant. In short, Cedar Bay would no longer be a cogeneration power plant.

This would appear to eliminate one of the public benefits taken into account by the Siting Board in its certification of the Cedar Bay power plant. It was understood during the certification process, based on information presented in the site certification application, that one of the benefits of the Cedar Bay cogeneration facility was its production of steam to generate electrical power and to use in an industrial process, thus effecting a saving in the cost of producing electrical power or process steam, or both.

Without prejudging all of the benefits and costs entailed in SCC's intention to become independent of Cedar Bay, it appears that such an action may require a modification of the certification order issued by the Siting Board to Cedar Bay. Furthermore, if the modification of the certification would, by removing Cedar Bay's cogeneration function, eliminate one of the public benefits of the original site certification, it may be necessary to consider whether SCC's proposed course of action in supplying its own steam requirements provides a public benefit to offset the loss of the cogeneration benefit. Certainly, it would not be a public benefit if the total air emissions from Cedar Bay and the SCC plant increased while the amount of power generated by Cedar Bay and the quantity of paper produced by the SCC plant remained the same.

Therefore the Department recommends that modification of the PSD permit should be postponed pending clarification by the Department of Environmental Protection of whether such an action requires a modification of the Cedar Bay site certification order.

Please keep us informed of action taken on this PSD permit modification request. Any questions regarding this matter may be referred to Paul Darst at (850) 922-1764.

Sincerely,

James L. Quinn

Chief, Bureau of State Planning

# **Best Available Copy**

LAW OFFICES

# OERTEL, HOFFMAN, FERNANDEZ & COLE, P.A.

301 SOUTH BRONOUGH STREET FIFTH FLOOR

TALLAHASSEE, FLORIDA 32301

MAILING ADDRESS:
POST OFFICE BOX 1110

TALLAHASSEE, FLORIDA 32302-1110

(850) 521-0700

FAX (850) 521-0720

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SEP U 3 1998

BUREAU OF AIR REGULATION

September 8, 1998

Syed Arif, P.E. Division of Air Department of Environmental Protection 2600 Blair Stone Road, MS-5505 Tallahassee, Florida 32399-2400

Re: DEP File No. 0310067-004-AC (PSD-FL-252)

Dear Mr. Arif:

TIMOTHY P. ATKINSON M. CHRISTOPHER BRYANT

TERRY COLE

C. ANTHONY CLEVELAND

SEGUNDO J. FERNANDEZ

DANIEL W. HARTMAN

KENNETH F. HOFFMAN KENNETH G. OERTEL PATRICIA A. RENOVITCH SCOTT SHIRLEY

This firm represents Stone Container Corporation respecting a requested modification to the PSD Permit for the Stone Jacksonville papermill, DEP File No. 0310067-004-AC (PSD-FL-252). Stone Container has received, and is in the process of formulating a response to, the Department of Environmental Protection's request for additional information dated August 4, 1998. You confirmed by telephone today that there is no time line currently running regarding Stone Container's response to the Department's request for additional information. I informed you that Stone Container will not have its response to the Department's request for additional information ready for at least another 30 days from today's date. You further confirmed that this delay would be acceptable within the present context.

If your understanding of these matters is other than as stated above, please contact me. In addition, please contact me should you have any other questions or comments.

Very truly yours,

Scott Shirlev

SS:cjb/F:\Document\SS\LTR\arif-1003-28.wpd

c: Al Koleff
John West
Joe Eskridge
David Buff

SEP U9 1998

BUREAU OF AIR REGULATION



# DEPARTMENT OF COMMUNITY AFFAIRS

"Helping Floridians create safe, vibrant, sustainable communities"

LAWTON CHILES
Governor

JAMES F. MURLEY Secretary

31 July 1998

RECEIVED

A A. Linero Administrator, New Source Review Department of Environmental Protection Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

AUG 04 1998

BUREAU OF AIR REGULATION

Dear Mr. Linero:

RE: Stone Container Corporation's application for a modification to their PSD permit

Thank you for informing us of the Stone Container Corporation (SCC) application for modification of its current Prevention of Significant Deterioration (PSD) permit. We have reviewed the excerpts from SCC's application which were attached to your letter of 15 July 1998.

SCC is currently operating a recycled fiber paper mill in Jacksonville, Florida, adjacent to the Cedar Bay cogeneration facility. The Cedar Bay facility burns coal to produce steam which is then used to generate electrical power. As a cogenerator, some of the steam is used for another purpose. In this case, it is sent next door to the SCC plant for use in the paper-making process. According to SCC, its paper plant required additional steam beyond the amount supplied by Cedar Bay and therefore three package boilers were installed at the paper plant to supply the additional steam. SCC obtained a PSD permit for these boilers in 1993. This permit was amended in 1995 to allow increased steam production from the three boilers (125,000 lbs/hr steam for each of the boilers).

Now SCC is seeking to amend the PSD permit again to allow each boiler to produce 150,000 lbs/hr steam. The attached PSD report states that "Although at present SCC anticipates that this increased level of steam production will be needed infrequently, such as during a scheduled outage by Cedar Bay, SCC would like to plan for the future independently of Cedar Bay."

Though the Department does not object to SCC's understandable desire to continue operating its paper plant during those periods when the Cedar Bay power plant is offline for a scheduled outage, SCC's stated intention to plan for the future independently of Cedar Bay appears to go further than this. It suggests a future scenario in which SCC would be burning fossil fuel to

2555 SHUMARD OAK BOULEVARD • TALLAHASSEE, FLORIDA 32399-2100

Phone: 850.488.8466/Suncom 278.8466 FAX: 850.921.0781/Suncom 291.0781 Internet address: http://www.state.fl.us/comaff/dca.html A.A. Linero 31 July 1998 Page 2

produce all of the steam it needs in the paper-making process—all of the time. Cedar Bay would also be burning fossil fuel to produce steam, but only for generation of electrical power—it would not be supplying steam to the SCC plant. In short, Cedar Bay would no longer be a cogeneration power plant.

This would appear to eliminate one of the public benefits taken into account by the Siting Board in its certification of the Cedar Bay power plant. It was understood during the certification process, based on information presented in the site certification application, that one of the benefits of the Cedar Bay cogeneration facility was its production of steam to generate electrical power and to use in an industrial process, thus effecting a saving in the cost of producing electrical power or process steam, or both.

Without prejudging all of the benefits and costs entailed in SCC's intention to become independent of Cedar Bay, it appears that such an action may require a modification of the certification order issued by the Siting Board to Cedar Bay. Furthermore, if the modification of the certification would, by removing Cedar Bay's cogeneration function, eliminate one of the public benefits of the original site certification, it may be necessary to consider whether SCC's proposed course of action in supplying its own steam requirements provides a public benefit to offset the loss of the cogeneration benefit. Certainly, it would not be a public benefit if the total air emissions from Cedar Bay and the SCC plant increased while the amount of power generated by Cedar Bay and the quantity of paper produced by the SCC plant remained the same.

Therefore the Department recommends that modification of the PSD permit should be postponed pending clarification by the Department of Environmental Protection of whether such an action requires a modification of the Cedar Bay site certification order.

Please keep us informed of action taken on this PSD permit modification request. Any questions regarding this matter may be referred to Paul Darst at (850) 922-1764.

Sincerely,

ames L. Quinn

Chief, Bureau of State Planning

JLQ/rpd

### REGULATORY & ENVIRONMENTAL SERVICES DEPARTMENT

### Air and Water Quality Division

July 31, 1998

Mr. Syed Arif
Department of Environmental Protection
Twin Towers Office Bldg.
2600 Blair Stone Rd.
Tallahassee, FL 32399-2400



AUG 04 1998

BUREAU OF AIR REGULATION

RE: Stone Container Corporation, Jacksonville, Three Steam Generating Boilers, PSD Determination

Dear Mr. Arif:

It is suggested that the following BACT Determinations from the RACT/BACT/LAER Clearinghouse seventh supplement be reviewed during your BACT determination for the referenced steam generating units:

ID Number	BACT for NOx (lbs/mmBtu)
AL 0093	0.0700
AL 0098	0.1000
GA 0063	0.1000 0.1500 *
MS 0029	0.1000
CA 0675	0.0330

<sup>\*</sup> Oil Fired

If you have any further questions concerning this issue or if we may be of further assistance, please contact Mr. Richard Robinson, P.E., of my staff at (904) 630-3484.

Very truly yours,

JLM/JEW/be

James L. Manning, P.E., Chief

c: Greg Radlinski, Esq, OGC Richard Robinson, P.E., AWQD AWQD File 0067-A

s:\permitv\0067bact.nox



# Department of Environmental Protection

Lawton Chiles Governor Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Virginia B. Wetherell Secretary

July 15, 1998

Distribution List Below

RE: Stone Container Corporation
Three Gas-Fired Package Boilers - Duval County

Attached are excerpts from an application submitted by Stone Container Corporation for a modification to their PSD permit to allow an increase in steam production rate from three gasfired boilers. The request by Stone Container may require modification of the Site Certification to the adjacent Cedar Bay Cogeneration Facility.

Please review and submit comments to the New Source Review Section, Bureau of Air Regulation, MS # 5505, 2600 Blairstone Road, Tallahasse, Florida 32399. The comments should be submitted by July 31, 1998, so they can be included in the Department's initial completeness review letter. If there are any questions regarding this matter, please call Syed Arif at (850) 921-9528.

for A. A. Linero, P.E.

New Source Review

AL/SA/t

cc: Buck Oven, PPS
Doug Roberts, HGS&S
Jim Antista, FG&F
David Russ, DCA
Earl Barker, S&B
Lawrence Curtin, H&K
Gregory Radlinski, C of J
Nancy Barnard, SJRWD
Rob Vandiver, FPSC
James Heard, Esq.
Lisa Cooper, M&P



# **Stone Container Corporation**

# Containerboard and Paper Division

P.O. Box 26998 Jacksonville, Florida 32226-6998

RECEIVED 904-751-6400

JUL 0**6 1998** 

**BUREAU OF** AIR REGULATION

July 2, 1998

Mr. A. A. Linero, P.E. Division of Air Resources Management Florida Department of Environmental Protection 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Stone Container Corporation, Jacksonville Mill Re: Proposed Package Boilers Steam Rate Increase

Dear Mr. Linero;

Please find enclosed with this letter a request to raise the permitted steam rates for the three package boilers located at our Jacksonville mill. Due to the potential increase in actual emissions, the project will be subject to prevention of significant deterioration (PSD) new source review. Four (4) copies of the air construction permit application are attached. Attached also is the permit review fee of \$7,500.

Please call if you need any additional information in order to issue a permit for this request.

Sincerely,

STONE CONTAINER CORPORATION

Jacksonville Mill

Ĵohn L. West.

General Manager

EPA NPS C. Helladay, BAR -

/maa

### **Stone Container Corporation**

invoice date/account	invoice reference		invoice amount	discount	net amount
6/18/98	061898	F 4503	7500.00	00	7500. 00
					\$7500.00 <b>*</b>
. , .	· .				;
,					
					. '

detach before presenting check for payment

### CHECK IS VOID IF COLORED BACKGROUND IS ABSENT.



# Stone Container Corporation

NationsBank Atlanta, Georgi 128239

9469 Eastport Road • Jacksonville, Florida, 32218

611

date

amount

7/03/98

\*\*\*7500 dollars and \*\*\*\*\*\*00

conte

\$7,500.00

PAY

Stone Container Corporation

FL DEPART OF ENVIR PROTECT.
TWIN TOWERS OFFICE BLDG
2600 BLAIR STONE ROAD
TALLAHASSE FL 323992400

dul



PSD APPLICATION
FOR
BOILER STEAM RATE INCREASE
STONE CONTAINER CORP.
JACKSONVILLE, FLORIDA

## **Prepared For:**

Stone Container Corp. 9469 East Port Road Jacksonville, Florida 32229

### **Prepared By:**

Golder Associates Inc. 6241 NW 23rd Street, Suite 500 Gainesville, Florida 32653-1500

June 1998 9837525Y\F1

# Department of Environmental Protection

### **DIVISION OF AIR RESOURCES MANAGEMENT**

### **APPLICATION FOR AIR PERMIT - LONG FORM**

See Instructions for Form No. 62-210.900(1)

### I. APPLICATION INFORMATION

This section of the Application for Air Permit form identifies the facility and provides general information on the scope and purpose of this application. This section also includes information on the owner or authorized representative of the facility (or the responsible official in the case of a Title V source) and the necessary statements for the applicant and professional engineer, where required, to sign and date for formal submittal of the Application for Air Permit to the Department. If the application form is submitted to the Department using ELSA, this section of the Application for Air Permit must also be submitted in hard-copy.

### **Identification of Facility Addressed in This Application**

Enter the name of the corporation, business, governmental entity, or individual that has ownership or control of the facility; the facility site name, if any; and the facility's physical location. If known, also enter the facility identification number.

Facility Owner/Company Name:	Stone Contai	ner Corporation	1
2. Site Name: Stone Container Corp	- Jacksonville	Mill	٠.
3. Facility Identification Number: 031	0067		[ ] Unknown
4. Facility Location Information: Street Address or Other Locator: City: Jacksonville	469 East Port County: Du	Road val	Zip Code: 32229
5. Relocatable Facility? [ ] Yes [x ] No		5. Existing Perr [X] Yes	mitted Facility? [ ] No
Application Processing Information (DEP	<u>Use)</u>		
1. Date of Receipt of Application:	O <sub>M</sub>	lux 6.	1998
2. Permit Number:	02	10067-	.004-AC
3. PSD Number (if applicable):	P51	)- FI -	252
4. Siting Number (if applicable):			

1

DEP Form No. 62.210.900(1) - Form Effective: 03-21-96

6/4/98

9837525Y/F1/CONST-AI

### Owner/Authorized Representative or Responsible Official

1. Name and Title of Owner/Authorized Representative or Responsible Official:

John L. West, General Manager

2. Owner/Authorized Representative or Responsible Official Mailing Address:

Organization/Firm: Stone Container Corporation

Street Address: PO Box 26998

City: Jacksonville

State: FL

Zip Code: 32226-6998

3. Owner/Authorized Representative or Responsible Official Telephone Numbers:

Telephone:

(904) 751-6400

Fax: (904) 751-5172

4. Owner/Authorized Representative or Responsible Official Statement:

I, the undersigned, am the owner or authorized representative\* of the non-Title Vsource addressed in this Application for Air Permit or the responsible official, as defined in Rule 62-210.200, F.A.C., of the Title V source addressed in this application, whichever is applicable. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements made in this application are true, accurate and complete and that, to the best of my knowledge, any estimates of emissions reported in this application are based upon reasonable techniques for calculating emissions. The air pollutant emissions units and air pollution control equipment described in this application will be operated and maintained so as to comply with all applicable standards for control of air pollutant emissions found in the statutes of the State of Florida and rules of the Department of Environmental Protection and revisions thereof. I understand that a permit, if granted by the Department, cannot be transferred without authorization from the Department, and I will promptly notify the Department upon sale or legal transfer of any permitted emissions unit.

Signature

7/2/98 Date

<sup>\*</sup> Attach letter of authorization if not currently on file.

### **Scope of Application**

This Application for Air Permit addresses the following emissions unit(s) at the facility. An Emissions Unit Information Section (a Section III of the form) must be included for each emissions unit listed.

Emissions Unit ID		sions Unit ID Description of Emissions Unit	
Unit #	Unit ID		
1R	022	Package Boiler No. 1	AC1A
2R	023	Package Boiler No. 2	AC1A
3R	026	Package Boiler No. 3	AC1A

See individual Emissions Unit (EU) sections for more detailed descriptions.

Multiple EU IDs indicated with an asterisk (\*). Regulated EU indicated with an "R".

3

DEP Form No. 62-210.900(1) - Form

Effective: 03-21-96

Permit

# Purpose of Application and Category

Check one (except as otherwise indicated):

# Category I: All Air Operation Permit Applications Subject to Processing Under Chapter 62-213, F.A.C.

This Application for Air Permit is submitted to obtain:

[	] Initial air operation permit under Chapter 62-213, F.A.C., for an existing facility which is classified as a Title V source.
[	] Initial air operation permit under Chapter 62-213, F.A.C., for a facility which, upon start up of one or more newly constructed or modified emissions units addressed in this application, would become classified as a Title V source.
	Current construction permit number:
[	] Air operation permit renewal under Chapter 62-213, F.A.C., for a Title V source.
	Operation permit to be renewed:
[	] Air operation permit revision for a Title V source to address one or more newly constructed or modified emissions units addressed in this application.
	Current construction permit number:
	Operation permit to be renewed:
[	] Air operation permit revision or administrative correction for a Title V source to address one or more proposed new or modified emissions units and to be processed concurrently with the air construction permit application. Also check Category III.
	Operation permit to be revised/corrected:
[	Air operation permit revision for a Title V source for reasons other than construction or modification of an emissions unit. Give reason for the revision e.g., to comply with a new applicable requirement or to request approval of an "Early Reductions" proposal.
	Operation permit to be revised:
	Reason for revision:
	<u> </u>

# Category II: All Air Construction Permit Applications Subject to Processing Under Rule 62-210.300(2)(b),F.A.C.

Th	is Application for Air Permit is submitted to obtain:
[	] Initial air operation permit under Rule 62-210.300(2)(b), F.A.C., for an existing facility seeking classification as a synthetic non-Title V source.
	Current operation/construction permit number(s):
[	] Renewal air operation permit under Rule 62-210.300(2)(b), F.A.C., for a synthetic non-Title V source.
	Operation permit to be renewed:
[	] Air operation permit revision for a synthetic non-Title V source. Give reason for revision; e.g.; to address one or more newly constructed or modified emissions units.
	Operation permit to be revised:
	Reason for revision:
Ca	tegory III: All Air Construction Permit Applications for All Facilities and Emissions Units.
Th	is Application for Air Permit is submitted to obtain:
[ x	] Air construction permit to construct or modify one or more emissions units within a facility (including any facility classified as a Title V source).
	Current operation permit number(s), if any:  N/A
[	] Air construction permit to make federally enforceable an assumed restriction on the potential emissions of one or more existing, permitted emissions units.
	Current operation permit number(s):
	eurent operation permit number(s).

	ne:	
[X ] Atta	eached - Amount: \$7,500.00 [ ] Not Applicable.	
Construc	ction/Modification Information	
1. Desc	cription of Proposed Project or Alterations:	_
	se in maximum permitted steam rate for Package Boilers Nos. 1-3 from 125,000 lb/hr steam.	000
		• .
2. Proje	ected or Actual Date of Commencement of Construction :	
	1 Jun 1998	•
3. Proje	ected Date of Completion of Construction:	
	1 Jun 1998	
	ional Engineer Cartification	
Professi	ional Engineer Certification	
1. Prof	fessional Engineer Name: David A. Buff gistration Number: 19011	

6

Fax: (352) 336-6603

DEP Form No. 62-210.900(1) - Form

Telephone: (352) 336-5600

3. Professional Engineer Telephone Numbers:

Effective: 03-21-96

#### 4. Professional Engineer's Statement:

I, the undersigned, hereby certify, except as particularly noted herein\*, that:

- (1) To the best of my knowledge, there is reasonable assurance that the air pollutant emissions unit(s) and the air pollution control equipment described in this Application for Air Permit, when properly operated and maintained, will comply with all applicable standards for control of air pollutant emissions found in the Florida Statutes and rules of the Department of Environmental Protection; and
- (2) To the best of my knowledge, any emission estimates reported or relied on in this application are true, accurate, and complete and are either based upon reasonable techniques available for calculating emissions or, for emission estimates of hazardous air pollutants not regulated for an emissions unit addressed in this application, based solely upon the materials, information and calculations submitted with this application.

If the purpose of this application is to obtain a Title V source air operation permit (check here [ ] if so), I further certify that each emissions unit described in this Application for Air Permit, when properly operated and maintained, will comply with the applicable requirements identified in this application to which the unit is subject, except those emissions units for which a compliance schedule is submitted with this application.

If the purpose of this application is to obtain an air construction permit for one or more proposed new or modified emissions units (check here [X] if so), I further certify that the engineering features of each such emissions unit described in this application have been designed or examined by me or individuals under my direct supervision and found to be in conformity with sound engineering principles applicable to the control of emissions of the air pollutants characterized in this application.

If the purpose of this application is to obtain an initial air operation permit or operation permit revision for one or more newly constructed or modified emissions units (check here [ ] if so), I further certify that, with the exception of any changes detailed as part of this application, each such emissions unit has been constructed or modified in substantial accordance with the information given in the corresponding application for air construction permit and with all provisions contained in such permit.

STEP David a biff	6/17/98
Signatures (seal)	Date

\*Attach any exception to certification statement.

#### **Application Contact**

1. Name and Title of Application Contact:

Joe Eskridge, Environmental Engineer

2. Application Contact Mailing Address:

Organization/Firm: Stone Container Corporation

Street Address: PO Box 26998

City: Jacksonville

State: FL

Zip Code: 32226-6998

3. Application Contact Telephone Numbers:

Telephone: (904) 751-6400

Fax: (904) 751-5822

#### **Application Comment**

6/4/98

#### II. FACILITY INFORMATION

#### A. GENERAL FACILITY INFORMATION

#### Facility Location and Type

1. Facility UTM Coordinates:

Zone: 17

East (km):

442.4

North (km): 3365.4

2. Facility Latitude/Longitude:

Latitude (DD/MM/SS):

30 / 25 / 15

Longitude: (DD/MM/SS): 81 / 36 / 0

6. Facility SIC(s):

3. Governmental

0

Facility Code:

4. Facility Status Code:

Α

5. Facility Major Group SIC Code:

26

2621

7. Facility Comment (limit to 500 characters):

#### Facility Contact

1. Name and Title of Facility Contact:

Joe Eskridge, Environmental Engineer

2. Facility Contact Mailing Address:

Organization/Firm: Stone Container Corporation

Street Address: PO Box 26998

City: Jacksonville

State: FL

Zip Code: 32226-6998

3. Facility Contact Telephone Numbers:

Telephone: (904) 751=6400

Fax:

(904) 751-5822

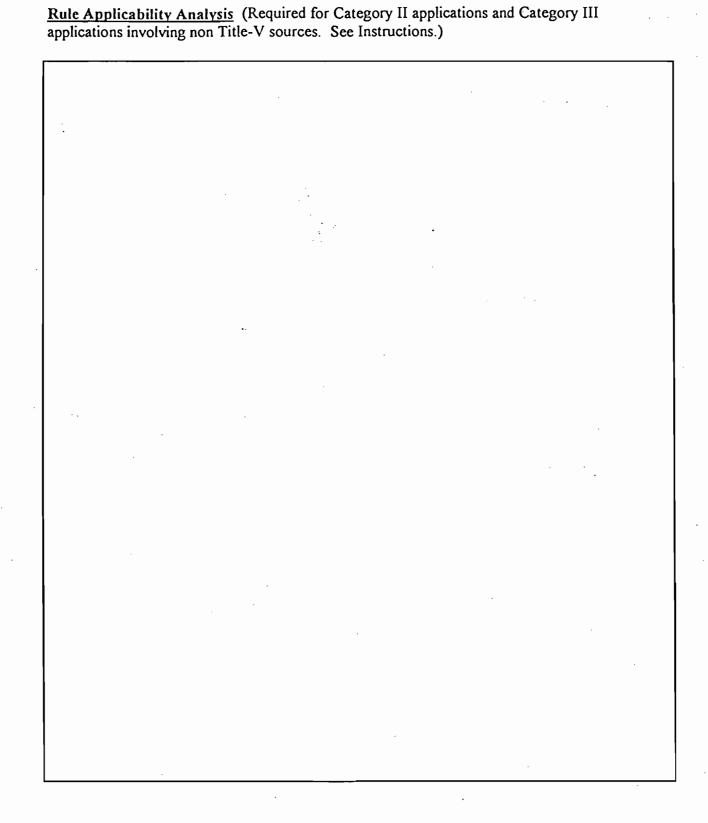
#### **Facility Regulatory Classifications**

Small Business Stationary Sou     [ ] Yes	ırce? [x ] No	[ ] Unknown
. 2. Title V Source? [ x ] Yes	[. ] No	,
Synthetic Non-Title V Source     [ ] Yes	? [ <b>x</b> ] No	
4. Major Source of Pollutants O  [ X ] Yes	ther than Hazardous Air Pollu [ ] No	utants (HAPs)?
5. Synthetic Minor Source of Po [ ] Yes	llutants Other than HAPs? [X] No	
6. Major Source of Hazardous A [ x ] Yes	ir Pollutants (HAPs)?	
7. Synthetic Minor Source of HA	APs? [x]No	
8. One or More Emissions Units [x] Yes	Subject to NSPS? [ ] No	
9. One or More Emissions Units [x] Yes	Subject to NESHAP? [ ] No	
10. Title V Source by EPA Desig	gnation? [x] No	
11. Facility Regulatory Classifica	tions Comment (limit to 200	characters):
Fac. is potentially subject to 4 source of HAPs due to potent fac. will be minor source.	IO CFR 61, Subpart M-NESHAF ial methanol emissions. If met	P for Asbestos. Fac. is major thanol is delisted as a HAP,

10

DEP Form No. 62.210.900(1) - Form Effective: 03-21-96

#### **B. FACILITY REGULATIONS**



11

DEP Form No. 62-210.900(1) - Form Effective: 03-21-96

4/22/96

9651021Y/F1/TVFI

List of Applicable Regulations (Required for Category I applications and Category III applications involving Title-V sources. See Instructions.)

Not Applicable		
·		
	•	
	·	
·		
		•
·		
		,
·		

#### C. FACILITY POLLUTANTS

### **Facility Pollutant Information**

15 Methanol A 2 Sulfur Dioxide SM	. Po	llutant Emitted		2	. Pollutant	Classification
	HAPs H115 SO2 NOx	Methanol Sulfur Dioxide	Pollutants			A SM
						× ·
						·

#### D. FACILITY POLLUTANT DETAIL INFORMATION

#### Facility Pollutant Detail Information:

1. 1	Pollutant Emitted:			
2. ]	Requested Emissions Cap:	(lb/hr)	(tons/yr)	
3. ]	Basis for Emissions Cap Code:		٠	
4. ]	Facility Pollutant Comment (limit	to 400 characters):		
			<u>,                                     </u>	

#### **Facility Pollutant Detail Information:**

1. Pollutant Emitted:			,
2. Requested Emissions Cap:	(lb/hr)	(tons/yr)	
3. Basis for Emissions Cap Code:			
4. Facility Pollutant Comment (limit	to 400 characters):		
	·		

#### E. FACILITY SUPPLEMENTAL INFORMATION

### Supplemental Requirements for All Applications

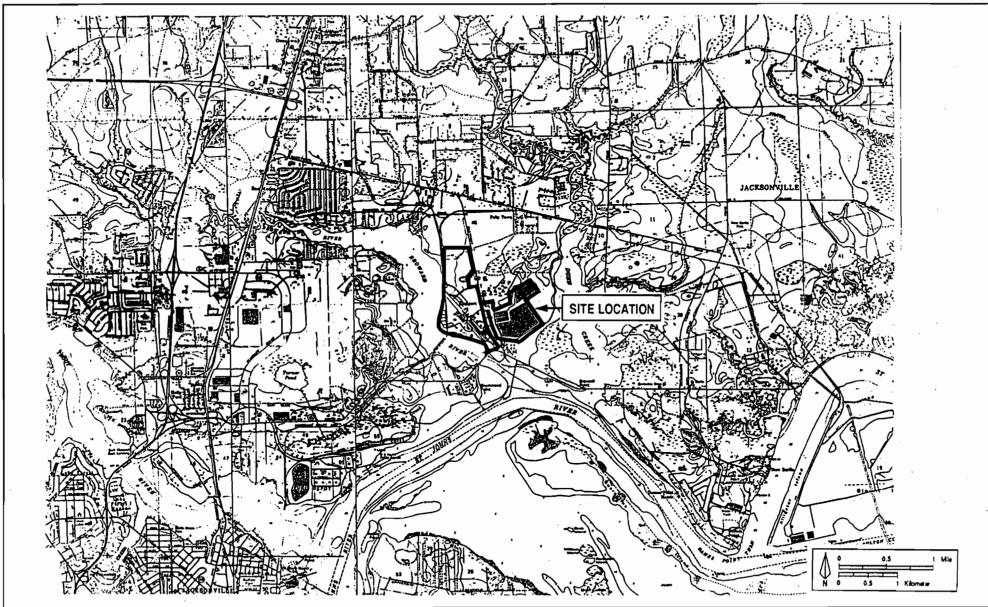
1. Area Map Showing Facility Location:  [ x ] Attached, Document ID: SCC-FE-1  [ ] Not Applicable [	] Waiver Requested
2. Facility Plot Plan:  [ x ] Attached, Document ID: SCC-FE-2  [ ] Not Applicable [	] Waiver Requested
3. Process Flow Diagram(s):  [ x ] Attached, Document ID(s): SCC-FE-3  [ ] Not Applicable [	- ] Waiver Requested
4. Precautions to Prevent Emissions of Unconfined Particula  [ ] Attached, Document ID:  [ x ] Not Applicable  [	nte Matter: - ] Waiver Requested
5. Fugitive Emissions Identification:  [ ] Attached, Document ID:  [ x ] Not Applicable [	] Waiver Requested
6. Supplemental Information for Construction Permit Applic  [ x ] Attached, Document ID: Attachment A  [ ] Not Applicable	·
Additional Supplemental Requirements for Category I Ap	oplications Only
7. List of Proposed Exempt Activities:  [ ] Attached, Document ID:  [ ] Not Applicable	-
8. List of Equipment/Activities Regulated under Title VI:  [ ] Attached, Document ID:  [ ] Equipment/Activities On site but Not Required to be [ ] Not Applicable	oe Individually Listed
9. Alternative Methods of Operation:  [ ] Attached, Document ID:  [ ] Not Applicable	
Alternative Modes of Operation (Emissions Trading):     Attached, Document ID:     Not Applicable	-

15

DEP Form No. 62-210.900(1) - Form Effective: 03-21-96

11. Identification of Additional Applicable Requirements:  [ ] Attached, Document ID:  [ ] Not Applicable
12. Compliance Assurance Monitoring Plan:
[ ] Attached, Document ID:
Not Applicable
13. Risk Management Plan Verification:
Plan Submitted to Implementing Agency - Verification Attached Document ID:
[ ] Plan to be Submitted to Implementing Agency by Required Date
[ ] Not Applicable
14. Compliance Report and Plan
Attached, Document ID:
Not Applicable
15. Compliance Statement (Hard-copy Required)
Attached, Document ID:
Not Applicable

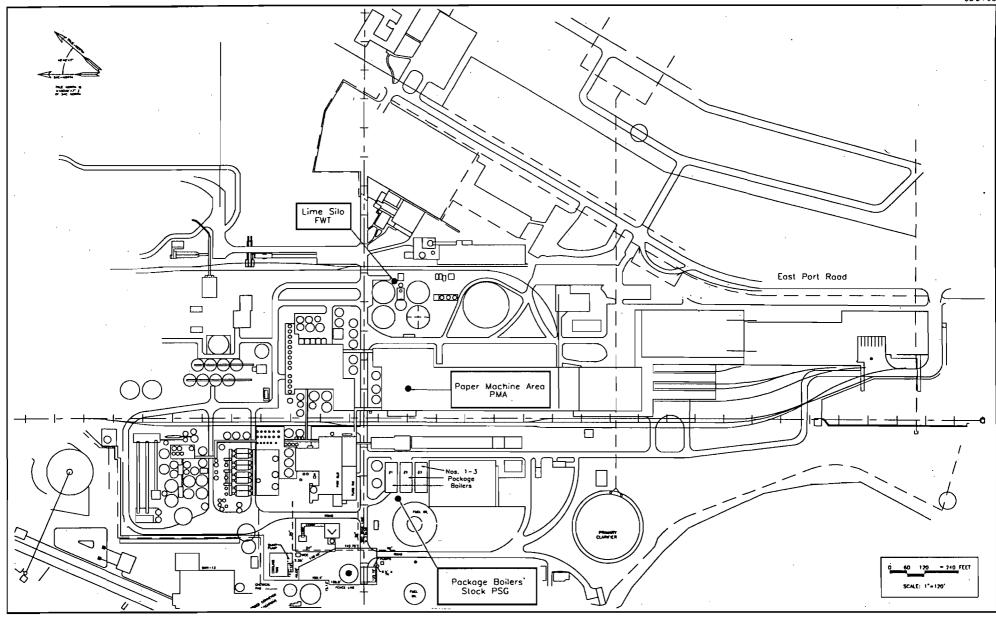
## ATTACHMENT SCC-FE-1 AREA MAP



Attachment SCC-FE-1 Site Location of Stone Container Corporation, Jacksonville



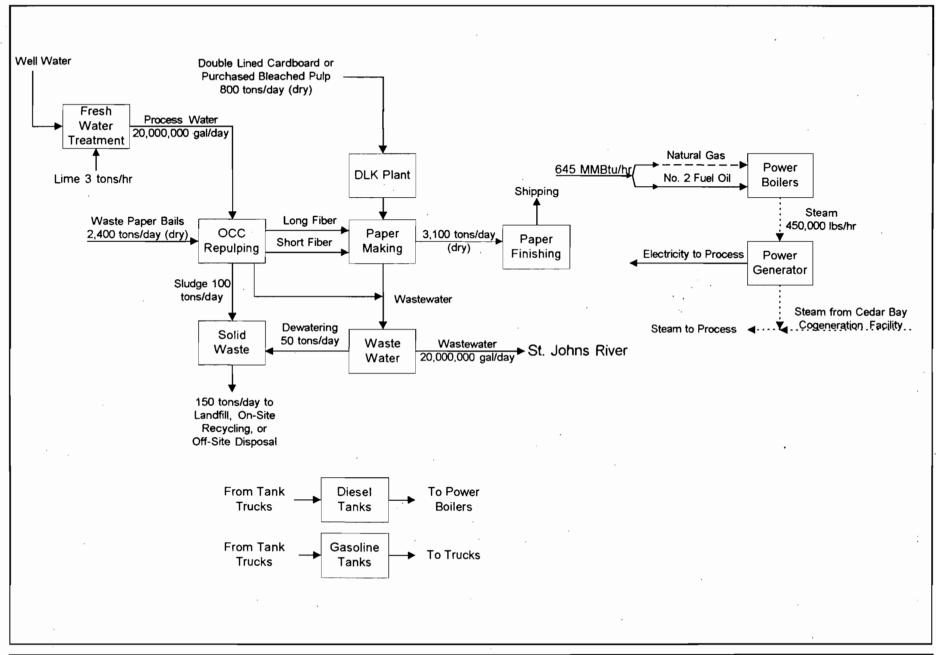
# ATTACHMENT SCC-FE-2 FACILITY PLOT PLAN



Attachment SCC-FE-2
Plot Plan of Stone Container Corporation Facility



# ATTACHMENT SCC-FE-3 PROCESS FLOW DIAGRAM



Process	Flow Legend
	Steam Flow
	Gas Flow
<b></b>	Solid / Liquid Flow

Stone Container
Corporation
Jacksonville, FL
Figure SCC-FD-3

	Emission Unit: FACILITY
	Process Area: FACILITY
	Filename: SCCFIG.VSD
	Latest Revision Date: 4/15/98 09:50 AM
-	



Engineering and Applied Sciences, Inc.

#### III. EMISSIONS UNIT INFORMATION

A separate Emissions Unit Information Section (including subsections A through L as required) must be completed for each emissions unit addressed in this Application for Air Permit. If submitting the application form in hard copy, indicate, in the space provided at the top of each page, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application. Some of the subsections comprising the Emissions Unit Information Section of the form are intended for regulated emissions units only. Others are intended for both regulated and unregulated emissions units. Each subsection is appropriately marked.

### A. TYPE OF EMISSIONS UNIT (Regulated and Unregulated Emissions Units)

#### Type of Emissions Unit Addressed in This Section

1. Regulated or Unregulated Emissions Unit? Check one:

[ x	] The emissions unit	addressed in th	is Emissions	Unit Information	Section is a	regulated
	emissions unit.					

[ ] The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.

2. Single Process, Group of Processes, or Fugitive Only? Check one:

[x] This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).

[ ] This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.

[ ] This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only

Emissions Unit Information Section 1	of <u>3</u>	Package Boiler No. 1
--------------------------------------	-------------	----------------------

### B. GENERAL EMISSIONS UNIT INFORMATION (Regulated and Unregulated Emissions Units)

#### **Emissions Unit Description and Status**

Description of Emission     Package Boiler No. 1	s Unit Addressed in This Section	(limit to 60 characters):
2. Emissions Unit Identifica	ation Number: [ ] No Corr	esponding ID [ ] Unknown
3. Emissions Unit Status Code: A	4. Acid Rain Unit? [ ] Yes [ X ] No	5. Emissions Unit Major Group SIC Code: 26
6. Emissions Unit Commen This boiler vents with tw	t (limit to 500 characters): to other boiler units to one commo	on stack.

#### **Emissions Unit Control Equipment Information**

A.

1. Description (limit to 200 characters):

**Low NOx Burners Burner Design** 

2. Control Device or Method Code; 24

В.

1. Description (limit to 200 characters):

2. Control Device or Method Code:

C.

1. Description (limit to 200 characters):

2. Control Device or Method Code:

### C. EMISSIONS UNIT DETAIL INFORMATION (Regulated Emissions Units Only)

#### **Emissions Unit Details**

1. Initial Startup Date: 3 Mar 1994	
2. Long-term Reserve Shutdown Date:	
Package Unit:     Manufacturer: ABB-Combustion Engineering	Model Number: 93104-20
4. Generator Nameplate Rating:	MW
5. Incinerator Information:	
Dwell Temperature:	°F
Dwell Time:	seconds
Incinerator Afterburner Temperature:	°F

#### **Emissions Unit Operating Capacity**

1. Maximum Heat Input Rate:		215	mmBtu/hr
2. Maximum Incineration Rate:	lbs/hr		tons/day
3. Maximum Process or Throughput	Rate:		
4. Maximum Production Rate:	150,000	lb/hr steam	1
5. Operating Capacity Comment (lim	nit to 200 characte	rs):	
200 MMBtu/hr maximum when firin natural gas.	g No. 2 fuel oil. 21	5 MMBtu/hr n	naximum when firing
			·

#### **Emissions Unit Operating Schedule**

Requested Maximum Operating Schedule:			
24	hours/day	7	days/week
52	weeks/yr	8,760	hours/yr

### D. EMISSIONS UNIT REGULATIONS (Regulated Emissions Units Only)

	•			
			-	
		-		
•				
		-		

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<u>List of Applicable Regulations</u> (Required for Category I applications and Category III applications involving Title-V sources. See Instructions.)

40 CFR 60 Appendix A 40 CFR 60.42b(a) 40 CFR 60.42b(g) 40 CFR 60.42b(j) 40 CFR 60.43b(g) 40 CFR 60.44b(a) 40 CFR 60.44b(b) 40 CFR 60.44b(h) 40 CFR 60.44b(i) 40 CFR 60.45b(a) 40 CFR 60.45b(j) 40 CFR 60.46b(a) 40 CFR 60.46b(c) 40 CFR 60.46b(d) 40 CFR 60.46b(e)(1) 40 CFR 60.46b(e)(4) 40 CFR 60.47b(f) 40 CFR 60.48b(a) 40 CFR 60.48b(b) 40 CFR 60.48b(c) 40 CFR 60.48b(d) 40 CFR 60.48b(e) 40 CFR 60.48b(f) 40 CFR 60.48b(g) 40 CFR 60.49b(a) 40 CFR 60.49b(b) 40 CFR 60.49b(d) 40 CFR 60.49b(f) 40 CFR 60.49b(g) 40 CFR 60.49b(h) 40 CFR 60.49b(i) 40 CFR 60.49b(j) 40 CFR 60.49b(o) 40 CFR 60.49b(r) 62-296.406(2) 62-296.406(3) 62-296.800(2)(a)3.

Emissions	Unit	Information	Section	_1	of	· 3	

Package Boiler No. 1

### E. EMISSION POINT (STACK/VENT) INFORMATION (Regulated Emissions Units Only)

#### **Emission Point Description and Type**

1		dentification of	Point on Plot	Plan	or Flow	Diagram:	
•		PSG				g. u	
2.	E	mission Point	Type Code:				· · · · · · · · · · · · · · · · · · ·
	[	] 1	[x ]2		[ ]3	[ ]	4
3.		Descriptions of the 100 character		ints C	omprising	g this Emissio	ons Unit for VE Tracking (limit
				•			
4.		D Numbers or	Descriptions (	of Em	ission Un	its with this	Emission Point in Common:
5.	] [	Discharge Type ] D ] R	Code: [ ] F [ x ] V	[	] H ] W	[ ]P	
6.	S	tack Height:				200	feet
7.	Е	Exit Diameter:	-			8	feet
8.	E	Exit Temperatu	re:			330	°F

<b>Source Information Section</b>	1	of 3	
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Package Boiler No. 1

9.	Actual Volumet	ric Flow Rate:	68,300	acfm
10.	Percent Water Vapor:			%
11.	Maximum Dry S	Standard Flow Rate:		dscfm
12.	Nonstack Emiss	ion Point Height:		feet
13.	Emission Point 1	UTM Coordinates:		
	Zone:	East (km):	North	(km):
14.	Emission Point	Comment (limit to 200	characters):	
			_	rameters above are total for all 2 fuel oil are: 345 deg. F; 67,149

<b>Emissions Unit Information Section</b>	1	of _	3	<del>_</del>	Package Boiler No.

## F. SEGMENT (PROCESS/FUEL) INFORMATION (Regulated and Unregulated Emissions Units)

Segment Description and Rate: Segment 1 of 2

<ol> <li>Segment Description (Process/Fuel Ty (limit to 500 characters):</li> </ol>	pe and Associated Operating Method/Mode)
External Combustion Boilers - Industria	l; natural Gas: over 100 MMBtu
2. Source Classification Code (SCC):	
. 1	-02-006-01
3. SCC Units:	
Million Cubic Feet Burned	-
4. Maximum Hourly Rate:	5. Maximum Annual Rate:
0.215	1,883
6. Estimated Annual Activity Factor:	
7. Maximum Percent Sulfur:	8. Maximum Percent Ash:
9. Million Btu per SCC Unit:	, ,
• •	1,000
10. Segment Comment (limit to 200 chars	acters):
-	actorsy.
Maximum Percent Sulfur = 0.001	
	·

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missions Unit Information Section 1 egment Description and Rate: Segmen	
	pe and Associated Operating Method/Mode)
2. Source Classification Code (SCC):	1-02-005-01
3 SCC Units: Thousand Ga	llons Burned
4. Maximum Hourly Rate: 1.449	5. Maximum Annual Rate: 10,750
6. Estimated Annual Activity Factor:	
7. Maximum Percent Sulfur: 0.05	8. Maximum Percent Ash: 0.1
9. Million Btu per SCC Unit:	,

Maximum combined yearly rate for Boiler No. 1, No. 2 and No. 3 is 10,750,000 gal/year.

## G. EMISSIONS UNIT POLLUTANTS (Regulated and Unregulated Emissions Units)

. Pollutant Emitted	Primary Control     Device Code	Secondary Control     Device Code	4. Pollutant Regulatory Code
SO2 NOx PM PM10	024		EL EL NS NS
co			NS
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			·
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### H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information**

1. Pollutant Emitted: so2						
2. Total Percent Efficiency of Control: %						
3. Potential Emissions: 10.43 lb/hour 38.7 tons/year						
4. Synthetically Limited? [x] Yes [] No						
5. Range of Estimated Fugitive/Other Emissions:						
[ ] 1 [ ] 2 [ ] 3 to tons/yr						
6. Emission Factor: 0.05 %S						
Reference: AP-42 and %S						
7. Emissions Method Code:						
[ <b>x</b> ]0 []1 []2 []3 []4 []5						
8. Calculation of Emissions (limit to 600 characters):						
1,449 gal/hr x 7.2 lb/gal x 0.0005 lb S/lb fuel x 2 lb SO2/lb S = 10.43 lbs/hr						
9. Pollutant Potential/Estimated Emissions Comment (limit to 200 characters):						
Annual SO2 emissions from #2 fuel oil firing for all 3 boilers shall not exceed 25 TPY, except during periods of natural gas unavailability, emissions shall not exceed 40 TPY with proper notification.						

#### Emissions Unit Information Section 1 of 3 Allowable Emissions (Pollutant identified on front page)

Α.

1.	Basis for Allowable Emissions Code:  OTHER
2.	Future Effective Date of Allowable Emissions:
3.	Requested Allowable Emissions and Units:
	0.05 % Sulfur
4.	Equivalent Allowable Emissions: 10.43 lb/hour 38.7 tons/year
5.	Method of Compliance (limit to 60 characters):
	Fuel Oil analysis
6.	Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode) (limit to 200 characters):
	See Attachment SCC-EU1-HA6. Maximum annual emissions under normal operations, when natural gas is available is 25 TPY. Emissions under natural gas curtailment cannot exceed 40 TPY.

B.

1.	Basis for Allowable Emissions Code:
2.	Future Effective Date of Allowable Emissions
3.	Requested Allowable Emissions and Units:
4.	Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance (limit to 60 characters):
6.	Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode) (limit to 200 characters):

<b>Emissions</b>	Unit Ir	formation	Section	1.	οf	3
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### H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information**:

1. Pollutant Emitted: NOx						
2. Total Percent Efficiency of Control: %						
3. Potential Emissions: 34.94 lb/hour 153.1 tons/year						
4. Synthetically Limited? [ ] Yes [x] No						
5. Range of Estimated Fugitive/Other Emissions:						
[ ] 1 [ ] 2 [ ] 3totons/yr						
6. Emission Factor: 0.2 lb/MMBtu						
Reference: Proposed Limit						
7. Emissions Method Code:						
[x]0 []1 []2 []3 []4 []5						
8. Calculation of Emissions (limit to 600 characters):						
NOx emissions capped at current permit limit. Equivalent to 0.1625 lb/MMBtu at max heat input.						
9. Pollutant Potential/Estimated Emissions Comment (limit to 200 characters):						
The maximum allowable NOx emissions shall not exceed 0.2 lb/MMBtu, 34.94 lbs/hr and 153.1 TPY per boiler. Total NOx emissions from all three boilers limited to 310 TPY.						

	wable Emissions (Pollutant identified	<u>on front</u>	page)	
۱.	· · · · · · · · · · · · · · · · · · ·			
1.	Basis for Allowable Emissions Code: OTHER			
2.	Future Effective Date of Allowable Emi	issions:		
3.	Requested Allowable Emissions and Un	nits:		
	0.2 lb/MMBtu			
1.	Equivalent Allowable Emissions:	34.94	lb/hour	<b>153.1</b> tons/year
5.	Method of Compliance (limit to 60 char	racters):		
	CEM for NOx			
<b>5</b> .	Pollutant Allowable Emissions Commer (limit to 200 characters):	nt (Desc.	of Related O	perating Method/Mode)
	Self-imposed limit by permittee. Based	on natura	ıl gas firing.	
	<b></b> , , ,			
3.	· .			
	Basis for Allowable Emissions Code			
	Basis for Allowable Emissions Code:			
1.		issions		
1.	Basis for Allowable Emissions Code:  Future Effective Date of Allowable Emi	issions:		
1 . 2 .	Future Effective Date of Allowable Emi			
1 . 2 .				
1 . 2 .	Future Effective Date of Allowable Emi			
2.	Future Effective Date of Allowable Emi		lb/hour	tons/year
1. 2. 3.	Future Effective Date of Allowable Emi Requested Allowable Emissions and Un Equivalent Allowable Emissions:	nits:	lb/hour	tons/year
2. 3.	Future Effective Date of Allowable Emi	nits:	lb/hour	tons/year
1. 2. 3.	Future Effective Date of Allowable Emissions and Un Requested Allowable Emissions and Un Equivalent Allowable Emissions:  Method of Compliance (limit to 60 char	nits:		
1. 2. 3.	Future Effective Date of Allowable Emi Requested Allowable Emissions and Un Equivalent Allowable Emissions:	nits:		

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#### H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information:**

1. Pollutant Emitted: PM						
2. Total Percent Efficiency of Control: %						
3. Potential Emissions: 2.9 lb/hour 11.5 tons/year						
4. Synthetically Limited? [x] Yes [] No						
5. Range of Estimated Fugitive/Other Emissions:						
[ ] 1						
6. Emission Factor: 2 lbs/1000 gal						
Reference: AP-42						
7. Emissions Method Code:						
[ ]0 [ ]1 [ ]2 [ <b>x</b> ]3 [ ]4 [ ]5						
8. Calculation of Emissions (limit to 600 characters):						
Fuel Oil: 1,449.3 gal/hr x 2 lbs/1000 gal = 2.90 lb/hr						
·						
9. Pollutant Potential/Estimated Emissions Comment (limit to 200 characters):						
See Attachment A for additional calculations						
See Attachment A for auditional calculations						

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1.	Basis for Allowable Emissions Code:		
2.	Future Effective Date of Allowable Emissions:	·	
3.	Requested Allowable Emissions and Units:		
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 characters):		
6.	Pollutant Allowable Emissions Comment (Desc. (limit to 200 characters):	of Related (	Operating Method/Mode)
В.			·
1.	Basis for Allowable Emissions Code:		
2.	Future Effective Date of Allowable Emissions:		
3.	Requested Allowable Emissions and Units:		
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 characters):		
6.	Pollutant Allowable Emissions Comment (Desc. (limit to 200 characters):	of Related (	Operating Method/Mode)

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	Emissions	Unit	Information	Section	1	of	3	
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### H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information**:

1. Pollutant Emitted: PM10	
2. Total Percent Efficiency of Control: %	
3. Potential Emissions: 1.45 lb/hour 6.1 tons/year	
4. Synthetically Limited? [x] Yes [] No	
5. Range of Estimated Fugitive/Other Emissions	
[ ] 1 [ ] 2 [ ] 3 to tons/yr	
6. Emission Factor: 50 % of PM	
Reference: AP-42	
7. Emissions Method Code:	
[ ]0	
8. Calculation of Emissions (limit to 600 characters):	
Fuel Oil: 2.90 lb/hr x 0.5 = 1.45 lb/hr	
9. Pollutant Potential/Estimated Emissions Comment (limit to 200 characters):	
See Attachment A for additional calculations	

Emissions Unit Information Section 1 of	3
Allowable Emissions (Pollutant identified on fro	nt page)

Allo A.	wable Emissions (Pollutant identified on front	: page)	
1.	Basis for Allowable Emissions Code:		
2.	Future Effective Date of Allowable Emissions:		
3.	Requested Allowable Emissions and Units:		
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 characters):		·
6.	Pollutant Allowable Emissions Comment (Desc. (limit to 200 characters):	of Related Ope	erating Method/Mode)
			·
			5555 <u>.</u>
В.	<u> </u>		·
1.	Basis for Allowable Emissions Code:		
2.	Future Effective Date of Allowable Emissions:		
3.	Requested Allowable Emissions and Units:		
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 characters):		
6.	Pollutant Allowable Emissions Comment (Desc. (limit to 200 characters):	of Related Ope	erating Method/Mode)

Emissions Unit Information Section 1	of	3
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### H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information**:

1. Pollutant Emitted: CO
2. Total Percent Efficiency of Control: %
3. Potential Emissions: 8.96 lb/hour 19 tons/year
4. Synthetically Limited? [ ] Yes [x] No
5. Range of Estimated Fugitive/Other Emissions:
[ ] 1
6. Emission Factor: 50 ppmvd
Reference: Test Data
7. Emissions Method Code:
[ ]0 [x]1 [ ]2 [ ]3 [ ]4 [ ]5
8. Calculation of Emissions (limit to 600 characters):
Natural Gas: 41,084 dscfm x 50 ppmvd x 60 min/hr x 2,116.8 lb/sq.ft. x (28/1545) lb-deg. R/ft-lb x 1/528 deg. R = 8.96 lb/hr
9. Pollutant Potential/Estimated Emissions Comment (limit to 200 characters):
Annual emissions based on 25 ppmvd. See Attachment A.

#### Emissions Unit Information Section 1 of 3 Allowable Emissions (Pollutant identified on front page)

Α.			·
1.	Basis for Allowable Emissions Code:		
2.	Future Effective Date of Allowable Emissions:		
3.	Requested Allowable Emissions and Units:	·	
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 characters):		
6.	Pollutant Allowable Emissions Comment (Desc. (limit to 200 characters):	of Related Operating N	fethod/Mode)
	•		
В.			
1.	Basis for Allowable Emissions Code:		
2.	Future Effective Date of Allowable Emissions:		
3.	Requested Allowable Emissions and Units:		
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 characters):		
6.	Pollutant Allowable Emissions Comment (Desc. (limit to 200 characters):	of Related Operating M	fethod/Mode)

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### I. VISIBLE EMISSIONS INFORMATION (Regulated Emissions Units Only)

	le Emissions Limitations: Visible Emissions Limitation 1 of 2
1.	Visible Emissions Subtype: VE05
2.	Basis for Allowable Opacity: [x ] Rule [ ] Other
3.	Requested Allowable Opacity Normal Conditions: 5 % Exceptional Conditions: % Maximum Period of Excess Opacity Allowed: min/hour
4.	Method of Compliance: EPA Method 9
5.	Visible Emissions Comment (limit to 200 characters): Natural gas firing; based on BACT
<u>'isib</u> 1.	le Emissions Limitations: Visible Emissions Limitation 2 of 2  Visible Emissions Subtype: VE10
2.	Basis for Allowable Opacity: [x] Rule [] Other
3.	Requested Allowable Opacity Normal Conditions: 10 % Exceptional Conditions: %
	Maximum Period of Excess Opacity Allowed: min/hour
4.	· · · · · · · · · · · · · · · · · · ·
<b>4</b> . <b>5</b> .	Maximum Period of Excess Opacity Allowed: min/hour  Method of Compliance:

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Emissions Unit	Information Section	1	ωſ	v
Limissions Citie	Amoi mation occion		•	

### J. CONTINUOUS MONITOR INFORMATION (Regulated Emissions Units Only)

Cont	inuous Monitoring System Continuou	us Monitor 1 of 1	
1.	Parameter Code: EM	2. Pollutant(s):	NOx
3.	CMS Requirement: [x ] Rule [ ]	Other	
4.	Monitor Information: Monitor Manufacturer: Servomex Model Number: 1491	Serial Number: 103	
5.	Installation Date: 01 Feb 1994		
6.	Performance Specification Test Date:	21 Jun 1994	
7.	Continuous Monitor Comment (limit to	o 200 characters):	,
l	CEMS for nitrogen oxides shall be oper requirements of 40 CFR 60.48b.	erated and maintained in accord	ance with
	·		
<u>Cont</u>	inuous Monitoring System Continuou	s Monitor of	
1.	Parameter Code:	2. Pollutant(s):	
3.	CMS Requirement: [ ] Rule [ ]	Other	
4.	Monitor Information: Monitor Manufacturer: Model Number:	Serial Number:	
5.	Installation Date:		·
6.	Performance Specification Test Date:		
7.	Continuous Monitor Comment (limit to	o 200 characters):	

<b>Emissions Unit Information Section</b>	1	of <sup>3</sup>
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### K. PREVENTION OF SIGNIFICANT DETERIORATION (PSD) INCREMENT TRACKING INFORMATION

(Regulated and Unregulated Emissions Units)

#### **PSD Increment Consumption Determination**

1. Increment Consuming for Particulate Matter or Sulfur Dioxide?

If the emissions unit addressed in this section emits particulate matter or sulfur dioxide, answer the following series of questions to make a preliminary determination as to whether or not the emissions unit consumes PSD increment for particulate matter or sulfur dioxide. Check the first statement, if any, that applies and skip remaining statements.

- The emissions unit is undergoing PSD review as part of this application, or has undergone PSD review previously, for particulate matter or sulfur dioxide. If so, emissions unit consumes increment.
   The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after January 6, 1975. If so, baseline emissions are zero, and the emissions unit consumes increment.
   The facility addressed in this application is classified as an EPA major source and the emissions unit began initial operation after January 6, 1975, but before December 27, 1977. If so, baseline emissions are zero, and the emissions unit consumes increment.
   For any facility, the emissions unit began (or will begin) initial operation after
- [ ] For any facility, the emissions unit began (or will begin) initial operation after December 27, 1977. If so, baseline emissions are zero, and emissions unit consumes increment.
- [ ] None of the above apply. If so, the baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

2. Increment Consuming for Nitrogen Dioxide?

If the emissions unit addressed in this section emits nitrogen oxides, answer the following series of questions to make a preliminary determination as to whether or not the emissions unit consumes PSD increment for nitrogen dioxide. Check first statement, if any, that applies and skip remaining statements.

- [x] The emissions unit addressed in this section is undergoing PSD review as part of this application, or has undergone PSD review previously, for nitrogen dioxide. If so, emissions unit consumes increment.
- [ ] The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after February 8, 1988. If so, baseline emissions are zero, and the source consumes increment.
- [ ] The facility addressed in this application is classified as an EPA major source and the emissions unit began initial operation after February 8, 1988, but before March 28, 1988. If so, baseline emissions are zero, and the source consumes increment.
- [ ] For any facility, the emissions unit began (or will begin) initial operation after March 28, 1988. If so, baseline emissions are zero, and the emissions unit consumes increment.
- [ ] None of the above apply. If so, baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

3.	Increment Consuming/E PM SO <sub>2</sub> NO <sub>2</sub>	[x]C [x]C [x]C	į į	E [ ] Unknown E [ ] Unknown E [ ] Unknown
4.	Baseline Emissions: PM SO <sub>2</sub> NO <sub>2</sub>	lb/hour lb/hour	· .	tons/year tons/year tons/year
5.	PSD Comment (limit to	200 characters):		

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### L. EMISSIONS UNIT SUPPLEMENTAL INFORMATION (Regulated Emissions Units Only)

#### Supplemental Requirements for All Applications

1.	Process Flow Diagram	
	[ x ] Attached, Document ID: SCC-EU1-L1         [ ] Not Applicable       [ ] Waiver Requested	
2.	Fuel Analysis or Specification	
	[ x ] Attached, Document ID: SCC-EU1-L2 [ ] Not Applicable [ ] Waiver Requested	
3.	Detailed Description of Control Equipment	
	[ ] Attached, Document ID:	
4.	Description of Stack Sampling Facilities	
	[ ] Attached, Document ID:	
5.	Compliance Test Report	
	[ ] Attached, Document ID: [x ] Not Applicable [ ] Previously Submitted, Date:	
6.	Procedures for Startup and Shutdown	
	[ ] Attached, Document ID: [x ] Not Applicable	•
7.	Operation and Maintenance Plan	
	[ ] Attached, Document ID: [x ] Not Applicable	
8.	Supplemental Information for Construction Permit Application	
	[X] Attached, Document ID: Attachment A [ ] Not Applicable	
9.	Other Information Required by Rule or Statute	
	[ ] Attached, Document ID: [X] Not Applicable	

Emissions	Unit :	Informa	tion	Section	1	of 3	
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#### Additional Supplemental Requirements for Category I Applications Only

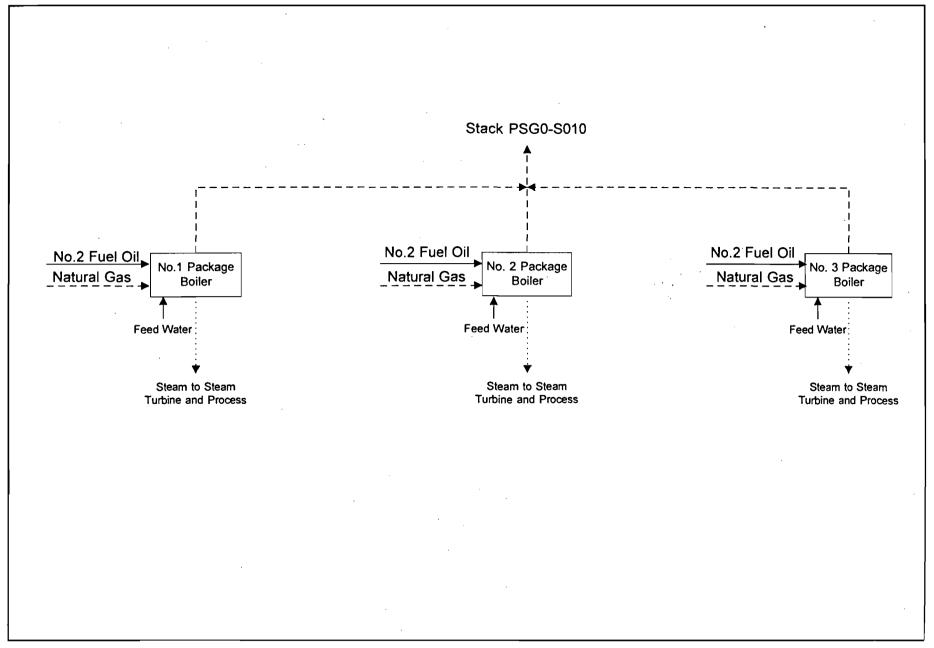
10.	Al	tern	native Methods of Operation
	[	]	Attached, Document ID: [ ] Not Applicable
11.	Al	tern	native Modes of Operation (Emissions Trading)
	[	]	Attached, Document ID: [ ] Not Applicable
12.	Id	enti	fication of Additional Applicable Requirements
•	[	]	Attached, Document ID: [ ] Not Applicable
13.	Co	omp	liance Assurance Monitoring Plan
	[	]	Attached, Document ID: [ ] Not Applicable
14.	A	cid F	Rain Permit Application (Hard Copy Required)
	[	]	Acid Rain Part - Phase II (Form No. 62-210.900(1)(a)) Attached, Document ID:
	[.	]	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.) Attached, Document ID:
	[	]	New Unit Exemption (Form No. 62-210.900(1)(a)2.) Attached, Document ID:
	[	]	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.) Attached, Document ID:
	[	]	Not Applicable

# ATTACHMENT SCC-EU1-HA6 POLLUTANT ALLOWABLE EMISSIONS COMMENT

## ATTACHMENT SCC-EU1-HA6 POLLUTANT ALLOWABLE EMISSIONS COMMENT

Boiler has SO<sub>2</sub> emission limit of 0.05% S fuel oil based on F.A.C. Rule 62-296.406, BACT, and 40 CFR Part 60, Subpart Db New Source Performance Standards. The BACT requires natural gas to be the primary fuel and the No. 2 fuel oil to be a maximum of 0.05 percent sulfur by weight. When using back up No. 2 fuel oil, emissions are limited to 25 TPY. If, due to factors beyond SCC, the limit is exceeded based on the unavailability of natural gas, then SCC shall provide a notice to the Department that will include a statement or reasons for the request to continue to burn No. 2 fuel oil. The emissions limit shall be less than 40 tons per year when burning No. 2 fuel oil. The notification of use of No. 2 fuel oil that causes emissions in excess of 25 TPY shall be published in a newspaper of general circulation in Jacksonville, Florida.

# ATTACHMENT SCC-EU1-L1 PROCESS FLOW DIAGRAM



Process	Flow Legend
	Steam Flow Gas Flow Solid / Liquid Flow

Stone Container Corporation Jacksonville, FL Figure SCC-EU1-L1

Emission Unit: PACKAGE BOILERS 1, 2, 3
Process Area: PACKAGE BOILERS 1, 2, 3
PIOCESS AFEB. TACIONOL BOILLING 1, 2, 3
Filename: SCCFIG.VSD Project: 9837525Y/F1
Latest Revision Date: 3/26/98 02:35 PM



# ATTACHMENT SCC-EU1-L2 FUEL ANALYSIS OR SPECIFICATION

#### **ATTACHMENT SCC-EU1-2**

## Package Boilers Fuel Analysis

Fuel	Density	Moisture	Weight	Weight %	Weight	Heat Capacity
	(lb/gal)	(%)	% Sulfur	Nitrogen	% Ash	
No. 2 Fuel Oil	7.2		0.05	·	0.1	138,000 BTU/gal
Natural Gas	_	_	.001	_		1000 BTU/ft <sup>3</sup>

#### III. EMISSIONS UNIT INFORMATION

A separate Emissions Unit Information Section (including subsections A through L as required) must be completed for each emissions unit addressed in this Application for Air Permit. If submitting the application form in hard copy, indicate, in the space provided at the top of each page, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application. Some of the subsections comprising the Emissions Unit Information Section of the form are intended for regulated emissions units only. Others are intended for both regulated and unregulated emissions units. Each subsection is appropriately marked.

### A. TYPE OF EMISSIONS UNIT (Regulated and Unregulated Emissions Units)

#### Type of Emissions Unit Addressed in This Section

1. Regulated or Unregulated Emissions Unit? Check one:

[ x	] The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.
[	] The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.

- 2. Single Process, Group of Processes, or Fugitive Only? Check one:
- [x] This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).

[	] This Emissions Unit Information Section addresses, as a single emissions unit, a group of
	process or production units and activities which has at least one definable emission point
	(stack or vent) but may also produce fugitive emissions.

] This Emissions Unit Information Section addresses, as a single emissions unit, one or more
process or production units and activities which produce fugitive emissions only.

Emissions	Unit	Information	Section	2	of	3	

### B. GENERAL EMISSIONS UNIT INFORMATION (Regulated and Unregulated Emissions Units)

#### **Emissions Unit Description and Status**

Description of Emission     Package Boiler No. 2	s Unit Addressed in This Section	(limit to 60 characters):
2. Emissions Unit Identific	ation Number: [ ] No Corr	esponding ID [ ] Unknown
3. Emissions Unit Status Code: A	4. Acid Rain Unit? [ ] Yes [ X ] No	5. Emissions Unit Major Group SIC Code: 26
6. Emissions Unit Commen This boiler vents with tw	t (limit to 500 characters): To other boiler units to one commo	on stack.

#### **Emissions Unit Control Equipment Information**

1	۱	
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1. Description (limit to 200 characters):

Low NOx Burners Burner Design

2. Control Device or Method Code: 24

В.

1. Description (limit to 200 characters):

2. Control Device or Method Code:

C.

1. Description (limit to 200 characters):

2. Control Device or Method Code:

### C. EMISSIONS UNIT DETAIL INFORMATION (Regulated Emissions Units Only)

#### **Emissions Unit Details**

1. Initial Startup Date: 3 Mar 1994	
2. Long-term Reserve Shutdown Date:	
Package Unit:     Manufacturer: ABB-Combustion Engineerin	g Model Number: 93104-20
4. Generator Nameplate Rating:	MW
5. Incinerator Information:  Dwell Temperature:  Dwell Time:  Incinerator Afterburner Temperature:	seconds

#### **Emissions Unit Operating Capacity**

1. Maximum Heat Input Rate:		215	mmBtu/hr					
2. Maximum Incineration Rate:	lbs/hr		tons/day					
3. Maximum Process or Throughput Rate:								
4. Maximum Production Rate:	150,000	lb/hr stean	n					
5. Operating Capacity Comment (lin	nit to 200 characte	ers):						
200 MMBtu/hr maximum when firin natural gas.	ng No. 2 fuel oil. 21	5 MMBtu/hr	maximum when firing					

#### **Emissions Unit Operating Schedule**

1. Requested Maximum Operating Schedule:							
24	hours/day	7	days/week				
52	weeks/yr	8,760	hours/yr				

### D. EMISSIONS UNIT REGULATIONS (Regulated Emissions Units Only)

<u>Rule Applicability Analysis</u> (Required for Category II Applications and Category III applications involving non Title-V sources. See Instructions.)

<u>List of Applicable Regulations</u> (Required for Category I applications and Category III applications involving Title-V sources. See Instructions.)

40 CFR 60 Appendix A 40 CFR 60.42b(a) 40 CFR 60.42b(g) 40 CFR 60.42b(j) 40 CFR 60.43b(g) 40 CFR 60.44b(a) 40 CFR 60.44b(b) 40 CFR 60.44b(h) 40 CFR 60.44b(i) 40 CFR 60.45b(a) 40 CFR 60.45b(j) 40 CFR 60.46b(a) 40 CFR 60.46b(c) 40 CFR 60.46b(d) 40 CFR 60.46b(e)(1) 40 CFR 60.46b(e)(4) 40 CFR 60.47b(f) 40 CFR 60.48b(a) 40 CFR 60.48b(b) 40 CFR 60.48b(c) 40 CFR 60.48b(d) 40 CFR 60.48b(e) 40 CFR 60.48b(f) 40 CFR 60.48b(g) 40 CFR 60.49b(a) 40 CFR 60.49b(b) 40 CFR 60.49b(d) 40 CFR 60.49b(f) 40 CFR 60.49b(g) 40 CFR 60.49b(h) 40 CFR 60.49b(i) 40 CFR 60.49b(j) 40 CFR 60.49b(o) 40 CFR 60.49b(r) 62-296.406(2) 62-296.406(3) 62-296.800(2)(a)3.

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Emissions Uni	t Information Section	2	οf	3
	· 2			

### E. EMISSION POINT (STACK/VENT) INFORMATION (Regulated Emissions Units Only)

#### **Emission Point Description and Type**

1.	]	Ide PS		cation	of Point on Plo	ot Plan	or Flow	Diagran	n:	
2.	]	Em	nissio	on Poin	t Type Code:	,				
		[	] 1		[ <b>x</b> ]2	•	[ ]3		[ ]	] 4
3.					of Emissions P ters per point)		Comprisin	g this E	missi	ons Unit for VE Tracking (limit
4.			Nur.	nbers o	or Descriptions	of Em	nission Ui	nits with	this	Emission Point in Common:
5.	]	Dis [ [	schar ] D ] R	)	pe Code: [ ]F [x]V	[ [	] H ] W	[	] P	
6.		Sta	ack I	Ieight:				20	00	feet
7.	]	Ex	it Di	ameter	·:				8	feet
8.	j	Ex	it Te	mpera	ture:		,		330	°F

Source Information Section	2	of	3	
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9.	Actual Volumet	ric Flow Rate:	68,300	acfm	
10.	Percent Water V	Vapor:		%	
11.	Maximum Dry S	Standard Flow Rate:		dscfm	
12.	Nonstack Emiss	ion Point Height:		feet	
13.	Emission Point	UTM Coordinates:			
	Zone:	East (km):	North	(km):	
14.	All three boilers	Comment (limit to 20) s exhaust into common tural gas. Parameters	ı stack. Stack pa		

Emissions <b>U</b>	Unit Information	Section	2	of	3	
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### F. SEGMENT (PROCESS/FUEL) INFORMATION (Regulated and Unregulated Emissions Units)

Segment Description and Rate: Segment \_\_\_\_ of \_\_\_\_

	•
1. Segment Description (Process/Fuel T (limit to 500 characters):	Type and Associated Operating Method/Mode)
External Combustion Boilers - Industr	ial; natural Gas: over 100 MMBtu
·	
2. Source Classification Code (SCC):	1-02-006-01
2. 800 H. 'a	
3. SCC Units:	
Million Cubic Feet Burned	<del></del>
4. Maximum Hourly Rate:	5. Maximum Annual Rate:
0.215	1,883
6. Estimated Annual Activity Factor:	
7. Maximum Percent Sulfur:	8. Maximum Percent Ash:
9. Million Btu per SCC Unit:	<u> </u>
y. Manon Did por Bee Cinc.	1,000
10. Segment Comment (limit to 200 cha	aracters):
Maximum Percent Sulfur = 0.001	•
	·

Segment Description and Rate: Segment 2 of 2

1. Segment Description (Process/Fuel Type and Associated Operating Method/Metho	ode)
(limit to 500 characters):	
External Combustion Boilers - Industrial; Distillate oil: over 100 MMBtu	

2. Source Classification Code (SCC):

1-02-005-01

3. SCC Units:

**Thousand Gallons Burned** 

4. Maximum Hourly Rate:

1.449

5. Maximum Annual Rate:

10,750

- 6. Estimated Annual Activity Factor:
- 7. Maximum Percent Sulfur:

0.05

8. Maximum Percent Ash:

9. Million Btu per SCC Unit:

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10. Segment Comment (limit to 200 characters):

Maximum combined yearly rate for Boiler No. 1, No. 2 and No. 3 is 10,750,000 gal/year.

### G. EMISSIONS UNIT POLLUTANTS (Regulated and Unregulated Emissions Units)

. Pollutant Emitted	Device Code 2. Primary Control 3.		4. Pollutant Regulatory Code		
SO2 NOx PM PM10 CO	024		EL EL NS NS		
	·				
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Emissions	Unit	Information	Section	2	of	3	
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### H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information**:

1. Pollutant Emitted: SO2	
2. Total Percent Efficiency of Control: %	
3. Potential Emissions: 10.43 lb/hour	38.7 tons/year
4. Synthetically Limited? [x] Yes [] No	
5. Range of Estimated Fugitive/Other Emissions:	
[ ]1 [ ]2 [ ]3toto	tons/yr
6. Emission Factor: 0.05 %S	
Reference: AP-42 and %S	
7. Emissions Method Code:	
[x]0 []1 []2 []3 []4	[ ]5
8. Calculation of Emissions (limit to 600 characters):	
1,449 gal/hr x 7.2 lb/gal x 0.0005 lb S/lb fuel x 2 lb SO2/lb S = 10.	43 lbs/hr
9. Pollutant Potential/Estimated Emissions Comment (limit to 200	characters):
Annual SO2 emissions from #2 fuel oil firing for all 3 boilers shall n during periods of natural gas unavailability, emissions shall not ex notification.	

<b>Emissions</b>	Unit Inform	nation Se	ction 2	2	of _	3
Allowable	<b>Emissions</b>	Pollutant	ident	ified on	front	page)

A.		
1.	Basis for Allowable Emissions Code: OTHER	
2.	2. Future Effective Date of Allowable Emissions:	
3.	3. Requested Allowable Emissions and Units:	
	0.05 % Sulfur	
4.	1. Equivalent Allowable Emissions: 10.43 lb/ho	our 38.7 tons/year
5.	5. Method of Compliance (limit to 60 characters):	
	Fuel Oil analysis	·
6.	5. Pollutant Allowable Emissions Comment (Desc. of Rel (limit to 200 characters):	lated Operating Method/Mode)
	See Attachment SCC-EU1-HA6. Maximum annual emiss when natural gas is available is 25 TPY. Emissions undexceed 40 TPY.	<del>-</del>
В.		•
.1.	1. Basis for Allowable Emissions Code:	
2.	2. Future Effective Date of Allowable Emissions:	
3:	B. Requested Allowable Emissions and Units:	·
4.	1. Equivalent Allowable Emissions lb/h	nour tons/year
5.	5 Method of Compliance (limit to 60 characters):	
6.	5. Pollutant Allowable Emissions Comment (Desc. of Re (limit to 200 characters):	elated Operating Method/Mode)

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### H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information**:

1. Pollutant Emitted: NOx
2. Total Percent Efficiency of Control: %
3. Potential Emissions: 34.94 lb/hour 153.1 tons/year
4. Synthetically Limited? [ ] Yes [x] No
5. Range of Estimated Fugitive/Other Emissions:
[ ] 1 [ ] 2 [ ] 3 to tons/yr
6. Emission Factor: 0.2 lb/MMBtu
Reference: Proposed Limit
7. Emissions Method Code:
[x]0 []1 []2 []3 []4 []5
8. Calculation of Emissions (limit to 600 characters):
NOx emissions capped at current permit limit. Equivalent to 0.1625 lb/MMBtu at max heat input.
9. Pollutant Potential/Estimated Emissions Comment (limit to 200 characters):
The maximum allowable NOx emissions shall not exceed 0.2 lb/MMBtu, 34.94 lbs/hr and 153.1 TPY per boiler. Total NOx emissions from all three boilers limited to 310 TPY.

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1		

Basis for Allowable Emissions Code: OTHER 2. Future Effective Date of Allowable Emissions: 3. Requested Allowable Emissions and Units: 0.2 lb/MMBtu 4. Equivalent Allowable Emissions: **34.94** lb/hour **153.1** tons/year 5. Method of Compliance (limit to 60 characters): **CEM for NOx** 6. Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode) (limit to 200 characters): Self-imposed limit by permittee. Based on natural gas firing.

В.

1. Basis for Allowable Emissions Code: 2. Future Effective Date of Allowable Emissions: 3. Requested Allowable Emissions and Units: 4. Equivalent Allowable Emissions: lb/hour tons/year 5. Method of Compliance (limit to 60 characters): 6. Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode) (limit to 200 characters):

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### H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information**:

1. Pollutant Emitted: PM	- 100 A
2. Total Percent Efficiency of Control: %	ó
3. Potential Emissions: 2.9 lb/hour	11.5 tons/year
4. Synthetically Limited? [x] Yes [] No	
5 Range of Estimated Fugitive/Other Emissions:	
[ ]1 [ ]2 [ ]3to	tons/yr
6. Emission Factor: 2 lb/1000 gal	
Reference: AP-42	
7. Emissions Method Code:	
[ ]0	[ ]5
8. Calculation of Emissions (limit to 600 characters):	
Fuel Oil: 1,449.3 gal/hr x 2 lbs/1000 gal = 2.90 lb/hr	
9 Pollutant Potential/Estimated Emissions Comment (limit to 2	200 characters)
See Attachment A for additional calculations	

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### Emissions Unit Information Section 2 of 3 Allowable Emissions (Pollutant identified on front page)

<b>A</b> .	wable Emissions (Pollutant identified on front	<u>pagej</u>	
1.	Basis for Allowable Emissions Code		
2.	Future Effective Date of Allowable Emissions:		
3.	Requested Allowable Emissions and Units:		
1.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 characters):		
5.	Pollutant Allowable Emissions Comment (Desc. (limit to 200 characters):	of Related Opera	ting Method/Mode)
3.		<u> </u>	
	Basis for Allowable Emissions Code:		
2.	Future Effective Date of Allowable Emissions		
3.	Requested Allowable Emissions and Units:		•
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
<b>-</b> 5.	Method of Compliance (limit to 60 characters):	<u> </u>	
_	Pollutant Allowable Emissions Comment (Desc.	of Dolored Ones	

(limit to 200 characters):

Emissions U	nit Information	Section	2	of	3

### H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information**:

1. Pollutant Emitted: PM10						
2. Total Percent Efficiency of Control: %						
3. Potential Emissions: 1.45 lb/hour 6.1 tons/year						
4. Synthetically Limited? [x] Yes [] No						
5. Range of Estimated Fugitive/Other Emissions:						
[ ] 1						
6. Emission Factor: 50 % of PM						
Reference: AP-42						
7. Emissions Method Code:						
[ ]0						
8. Calculation of Emissions (limit to 600 characters):  Fuel Oil: 2.90 lb/hr x 0.5 = 1.45 lb/hr						
9. Pollutant Potential/Estimated Emissions Comment (limit to 200 characters):  See Attachment A for additional calculations						
ess Attachment A for additional entoniations						

### Emissions Unit Information Section 2 of 3 Allowable Emissions (Pollutant identified on front page)

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\llo	wable Emissions (Pollutant identified o	n front page)	
A.		Bes	t Available Copy
1.	Basis for Allowable Emissions Code:		
2.	Future Effective Date of Allowable Emiss	sions:	· · · · · · · · · · · · · · · · · · ·
3.	Requested Allowable Emissions and Unit	S:	
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 charac	cters):	
6.	Pollutant Allowable Emissions Comment (limit to 200 characters):	(Desc. of Related Oper	ating Method/Mode)
В.			
1.	Basis for Allowable Emissions Code:		
2.	Future Effective Date of Allowable Emiss	sions:	
3.	Requested Allowable Emissions and Unit	s:	
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 chara	cters):	

6. Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode)

(limit to 200 characters):

Emissions	Unit	Information	Section	2	of	3	

### H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information**:

1. Pollutant Emitted: CO						
2. Total Percent Efficiency of Control: %						
3. Potential Emissions: 8.96 lb/hour 19 tons/year						
4. Synthetically Limited? [ ] Yes [x] No						
5. Range of Estimated Fugitive/Other Emissions:						
[ ] 1 [ ] 2 [ ] 3 to tons/yr						
6. Emission Factor: 50 ppmvd						
Reference: Test Data						
7. Emissions Method Code:						
[ ]0 [x]1 [ ]2 [ ]3 [ ]4 [ ]5						
8. Calculation of Emissions (limit to 600 characters):						
Natural Gas: 41,084 dscfm x 50 ppmvd x 60 min/hr x 2,116.8 lb/sq.ft. x (28/1545) lb-deg. R/ft-lb x 1/528 deg. R = 8.96 lb/hr $\sim$						
9. Pollutant Potential/Estimated Emissions Comment (limit to 200 characters):  Annual emissions based on 25 ppmvd. See Attachment A.						
· · · · · · · · · · · · · · · · · · ·						

# Emissions Unit Information Section 2 of 3 Allowable Emissions (Pollutant identified on front page)

<u> </u>	wable Emissions (Pollutant identified on front	<u>page)</u>	
1.	Basis for Allowable Emissions Code:		
2.	Future Effective Date of Allowable Emissions:		·
3.	Requested Allowable Emissions and Units:		
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 characters):		
6.	Pollutant Allowable Emissions Comment (Desc. (limit to 200 characters):	of Related Operati	ng Method/Mode)
В.	•		
1.	Basis for Allowable Emissions Code:		
2.	Future Effective Date of Allowable Emissions:		
3.	Requested Allowable Emissions and Units:		
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 characters):	,	
6.	Pollutant Allowable Emissions Comment (Desc. (limit to 200 characters):	of Related Operati	ng Method/Mode)

## I. VISIBLE EMISSIONS INFORMATION (Regulated Emissions Units Only)

1.	Visible Emissions Subtype: VE05
2.	Basis for Allowable Opacity: [x ] Rule [ ] Other
3.	Requested Allowable Opacity Normal Conditions: 5 % Exceptional Conditions: % Maximum Period of Excess Opacity Allowed: min/hour
4.	Method of Compliance: EPA Method 9
5.	Visible Emissions Comment (limit to 200 characters): Natural gas firing; based on BACT
	·
	le Emissions Limitations: Visible Emissions Limitation 2 of 2
1.	Visible Emissions Subtype: VE10
1.	Visible Emissions Subtype: VE10
1. 2.	Visible Emissions Subtype: VE10  Basis for Allowable Opacity: [x] Rule [] Other  Requested Allowable Opacity Normal Conditions: 10 % Exceptional Conditions: %
1. 2. 3.	Visible Emissions Subtype: VE10  Basis for Allowable Opacity: [x] Rule [] Other  Requested Allowable Opacity Normal Conditions: 10 % Exceptional Conditions: % Maximum Period of Excess Opacity Allowed: min/hour  Method of Compliance:

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Emissions Unit Information Section		of	

## J. CONTINUOUS MONITOR INFORMATION (Regulated Emissions Units Only)

Continuous Monitoring System Continuous Monitor 1 of 1			
1.	Parameter Code: EM	2. Pollutant(s):	NOx
3.	CMS Requirement: [x ] Rule [ ] Other		
4.	Monitor Information: Monitor Manufacturer: Servomex Model Number: 1491	Serial Number: 103	
5.	Installation Date: 01 Feb 1994		
6.	Performance Specification Test Date:	21 Jun 1994	
7.	7. Continuous Monitor Comment (limit to 200 characters):  CEMS for nitrogen oxides shall be operated and maintained in accordance with requirements of 40 CFR 60.48b.		
-		•	
	inuous Monitoring System Continuou		
1.	Parameter Code:	2. Pollutant(s):	
3.	CMS Requirement: [ ] Rule [ ] Other		
4.	Monitor Information: Monitor Manufacturer: Model Number:	Serial Number:	
5.	Installation Date:		
6.	Performance Specification Test Date:		
7.	7. Continuous Monitor Comment (limit to 200 characters):		
	•		

### K. PREVENTION OF SIGNIFICANT DETERIORATION (PSD) INCREMENT TRACKING INFORMATION

(Regulated and Unregulated Emissions Units)

#### **PSD Increment Consumption Determination**

1. Increment Consuming for Particulate Matter or Sulfur Dioxide?

If the emissions unit addressed in this section emits particulate matter or sulfur dioxide, answer the following series of questions to make a preliminary determination as to whether or not the emissions unit consumes PSD increment for particulate matter or sulfur dioxide. Check the first statement, if any, that applies and skip remaining statements.

- [x] The emissions unit is undergoing PSD review as part of this application, or has undergone PSD review previously, for particulate matter or sulfur dioxide. If so, emissions unit consumes increment.
- [ ] The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after January 6, 1975. If so, baseline emissions are zero, and the emissions unit consumes increment.
- [ ] The facility addressed in this application is classified as an EPA major source and the emissions unit began initial operation after January 6, 1975, but before December 27, 1977. If so, baseline emissions are zero, and the emissions unit consumes increment.
- For any facility, the emissions unit began (or will begin) initial operation after December 27, 1977. If so, baseline emissions are zero, and emissions unit consumes increment.
- [ ] None of the above apply. If so, the baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

2. Increment Consuming for Nitrogen Dioxide?

If the emissions unit addressed in this section emits nitrogen oxides, answer the following series of questions to make a preliminary determination as to whether or not the emissions unit consumes PSD increment for nitrogen dioxide. Check first statement, if any, that applies and skip remaining statements.

- [x] The emissions unit addressed in this section is undergoing PSD review as part of this application, or has undergone PSD review previously, for nitrogen dioxide. If so, emissions unit consumes increment.
- [ ] The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after February 8, 1988. If so, baseline emissions are zero, and the source consumes increment.
- [ ] The facility addressed in this application is classified as an EPA major source and the emissions unit began initial operation after February 8, 1988, but before March 28, 1988. If so, baseline emissions are zero, and the source consumes increment.
- [ ] For any facility, the emissions unit began (or will begin) initial operation after March 28, 1988. If so, baseline emissions are zero, and the emissions unit consumes increment.
- [ ] None of the above apply. If so, baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

3.	Increment Consuming/E: PM SO <sub>2</sub> NO <sub>2</sub>	[x ] C [x ] C [x ] C	[ ]E [ ]E	[ ] Unknown
4.	Baseline Emissions: PM SO <sub>2</sub> NO <sub>2</sub>	lb/hour lb/hour		tons/year tons/year tons/year
5.	PSD Comment (limit to	200 characters):		

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### L. EMISSIONS UNIT SUPPLEMENTAL INFORMATION (Regulated Emissions Units Only)

### **Supplemental Requirements for All Applications**

1.	Process Flow Diagram
•	[ X ] Attached, Document ID:       SCC-EU1-L1         [ ] Not Applicable       [ ] Waiver Requested
2.	Fuel Analysis or Specification
	[ x ] Attached, Document ID: SCC-EU1-L2         [ ] Not Applicable       [ ] Waiver Requested
3.	Detailed Description of Control Equipment
	[ ] Attached, Document ID: [x ] Not Applicable [ ] Waiver Requested
4.	Description of Stack Sampling Facilities
	[ ] Attached, Document ID:
5.	Compliance Test Report
	[ ] Attached, Document ID: [x ] Not Applicable [ ] Previously Submitted, Date:
6.	Procedures for Startup and Shutdown
	[ ] Attached, Document ID: [x ] Not Applicable
7.	Operation and Maintenance Plan
	[ ] Attached, Document ID: [x ] Not Applicable
8.	Supplemental Information for Construction Permit Application
	[X] Attached, Document ID: Attachment A [ ] Not Applicable
9.	Other Information Required by Rule or Statute
	[ ] Attached, Document ID: [x ] Not Applicable

### Additional Supplemental Requirements for Category I Applications Only

10.	Alte	em	ative Methods of Operation
	[	]	Attached, Document ID: [ ] Not Applicable
11.	Alte	ern	ative Modes of Operation (Emissions Trading)
	[	]	Attached, Document ID: [ ] Not Applicable
12.	Ider	ntif	ication of Additional Applicable Requirements
	[	]	Attached, Document ID: [ ] Not Applicable
13.	Con	npl	liance Assurance Monitoring Plan
	[	]	Attached, Document ID: [ ] Not Applicable
14.	Acie	d F	Rain Permit Application (Hard Copy Required)
	[	]	Acid Rain Part - Phase II (Form No. 62-210.900(1)(a)) Attached, Document ID:
	[	]	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.) Attached, Document ID:
	[	]	New Unit Exemption (Form No. 62-210.900(1)(a)2.) Attached, Document ID:
	[	]	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.) Attached, Document ID:
	[	]	Not Applicable

#### III. EMISSIONS UNIT INFORMATION

A separate Emissions Unit Information Section (including subsections A through L as required) must be completed for each emissions unit addressed in this Application for Air Permit. If submitting the application form in hard copy, indicate, in the space provided at the top of each page, the number of this Emissions Unit Information Section and the total number of Emissions Unit Information Sections submitted as part of this application. Some of the subsections comprising the Emissions Unit Information Section of the form are intended for regulated emissions units only. Others are intended for both regulated and unregulated emissions units. Each subsection is appropriately marked.

#### A. TYPE OF EMISSIONS UNIT (Regulated and Unregulated Emissions Units)

Type of Emissions Unit Addressed in This Section	
1. Regulated or Unregulated Emissions Unit? Check one:	
[x] The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.	
[ ] The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.	
2. Single Process, Group of Processes, or Fugitive Only? Check one:	
[x] This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).	h
[ ] This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.	
[ ] This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only	

Emissions U	nit Information	Section	3	of	3

# B. GENERAL EMISSIONS UNIT INFORMATION (Regulated and Unregulated Emissions Units)

### **Emissions Unit Description and Status**

1.	Description of Emission  Package Boiler No. 3	s Unit Addressed in This Section	(limit to 60 characters):
2.	Emissions Unit Identific	ation Number: [ ] No Corre	esponding ID [ ] Unknown
3.	Emissions Unit Status Code: A	4. Acid Rain Unit? [ ] Yes [ X ] No	5. Emissions Unit Major Group SIC Code: 26
6.		t (limit to 500 characters): To other boiler units to one commo	on stack.

#### **Emissions Unit Control Equipment Information**

A.

1. Description (limit to 200 characters):

Low NOx Burners Burner Design

2. Control Device or Method Code: 24

В.

1. Description (limit to 200 characters):

2. Control Device or Method Code:

C.

1. Description (limit to 200 characters):

2. Control Device or Method Code:

## C. EMISSIONS UNIT DETAIL INFORMATION (Regulated Emissions Units Only)

#### **Emissions Unit Details**

1.	Initial Startup Date: 3 Mar 1994		
2.	Long-term Reserve Shutdown Date:	· 	
3.	Package Unit: Manufacturer: ABB-Combustion Engineering	Model Number: 93104-20	
4.	Generator Nameplate Rating:	MW	
5.	Incinerator Information:  Dwell Temperature:  Dwell Time: Incinerator Afterburner Temperature:	°F seconds °F	

#### **Emissions Unit Operating Capacity**

Maximum Heat Input Rate:		215	mmBtu/hr
2. Maximum Incineration Rate:	lbs/hr		tons/day
3. Maximum Process or Throughput Ra	ite:		
4. Maximum Production Rate:	150,000	lb/hr steam	
5. Operating Capacity Comment (limit t	o 200 characte	rs):	
200 MMBtu/hr maximum when firing N natural gas.	o. 2 fuel oil. 21	5 MMBtu/hr m	aximum when firing

### **Emissions Unit Operating Schedule**

1. Requested Maximum Operating Schedule:								
24	hours/day	7	days/week					
52	weeks/yr	8,760	hours/yr					

### D. EMISSIONS UNIT REGULATIONS (Regulated Emissions Units Only)

				-	
			·		
	·				
					·
		:			
		•			

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<u>List of Applicable Regulations</u> (Required for Category I applications and Category III applications involving Title-V sources. See Instructions.)

40 CFR 60 Appendix A 40 CFR 60.42b(a) 40 CFR 60.42b(g) 40 CFR 60.42b(j) 40 CFR 60.43b(g) 40 CFR 60.44b(a) 40 CFR 60.44b(b) 40 CFR 60.44b(h) 40 CFR 60.44b(i) 40 CFR 60.45b(a) 40 CFR 60.45b(j) 40 CFR 60.46b(a) 40 CFR 60.46b(c) 40 CFR 60.46b(d) 40 CFR 60.46b(e)(1) 40 CFR 60.46b(e)(4) 40 CFR 60.47b(f) 40 CFR 60.48b(a) 40 CFR 60.48b(b) 40 CFR 60.48b(c) 40 CFR 60.48b(d) 40 CFR 60.48b(e) 40 CFR 60.48b(f) 40 CFR 60.48b(g) 40 CFR 60.49b(a) 40 CFR 60.49b(b) 40 CFR 60.49b(d) 40 CFR 60.49b(f) 40 CFR 60.49b(g) 40 CFR 60.49b(h) 40 CFR 60.49b(i) 40 CFR 60.49b(j) 40 CFR 60.49b(o) 40 CFR 60.49b(r) 62-296.406(2) 62-296.406(3) 62-296.800(2)(a)3.

Emissions	Unit	Information	Section	3	of	3

# E. EMISSION POINT (STACK/VENT) INFORMATION (Regulated Emissions Units Only)

#### **Emission Point Description and Type**

1.	Identification of PSG	Point on Plo	ot Plan or Flow	Diagram:	
2.	Emission Point	Type Code:			
	[ ]1	[x]2	[ ]3	[ ]	4
3.	Descriptions of to 100 characte			g this Emissic	ons Unit for VE Tracking (limit
		·			
4.	ID Numbers or 22,23	Descriptions	of Emission U	nits with this I	Emission Point in Common:
5.	Discharge Type  [ ] D  [ ] R	Code: [ ]F [x]V	[ ]H [ ]W	[ ]P	
6.	Stack Height:			200	feet
7.	Exit Diameter:			8	feet
8.	Exit Temperatu	re:		330	°F

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Source	<b>Information</b>	Section	3		of	3	
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9.	Actual Volumetric Flow Rate: 68,300 acfm				
10.	Percent Water	Vapor:		%	
11.	Maximum Dry	Standard Flow Rate:		dscfm	
12.	Nonstack Emiss	sion Point Height:		feet	
13.	Emission Point	UTM Coordinates:			
	Zone:	East (km):	North	(km):	
14.	Emission Point	Comment (limit to 200 charact	ters):		
		s exhaust into common stack. S urning natural gas. Parameters		rameters above are total for all 2 fuel oil are: 345 deg. F; 67,149	

<b>Emissions Unit In</b>	formation Secti	on <u>3</u>	_ of _	3
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# F. SEGMENT (PROCESS/FUEL) INFORMATION (Regulated and Unregulated Emissions Units)

Segment Description and Rate: Segment \_\_\_\_ of \_\_\_2

1. Segment Description (Process/Fuel Type and Associated Operating Method/Mode) (limit to 500 characters):								
External Combustion Boilers - Industrial; natural Gas: over 100 MMBtu								
-								
•								
<i></i>								
2. Source Classification Code (SCC):								
1	-02-006-01							
3. SCC Units:								
Million Cubic Feet Burned								
4. Maximum Hourly Rate:	5. Maximum Annual Rate:							
0.215	1,883							
6. Estimated Annual Activity Factor:								
7. Maximum Percent Sulfur:	8. Maximum Percent Ash:							
9. Million Btu per SCC Unit:								
	1,000							
10. Segment Comment (limit to 200 chara	acters):							
	•							

Segment Description and Rate: Segment 2 of 2

Fyte	nal Combustion Boilers - Industrial: Distillate oil: over 100 MMBtu
(lin	it to 500 characters):
1. Seg	ment Description (Process/Fuel Type and Associated Operating Method/Mode)

2. Source Classification Code (SCC):

1-02-005-01

3. SCC Units:

**Thousand Gallons Burned** 

4. Maximum Hourly Rate:

5. Maximum Annual Rate:

10,750

6. Estimated Annual Activity Factor:

7. Maximum Percent Sulfur:

0.05

1.449

8. Maximum Percent Ash:

0.1

9. Million Btu per SCC Unit:

138

10. Segment Comment (limit to 200 characters):

Maximum combined yearly rate for Boiler No. 1, No. 2 and No. 3 is 10,750,000 gal/year.

### G. EMISSIONS UNIT POLLUTANTS (Regulated and Unregulated Emissions Units)

. Pollutant Emitted	Primary Control     Device Code	Secondary Control     Device Code	4. Pollutant Regulatory Code		
SO2 NOX PM PM10 CO	024	<i>;</i>	EL EL NS NS NS		
-					

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## H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information**:

Pollutant Emitted: SO2
2. Total Percent Efficiency of Control: %
3. Potential Emissions: 10.43 lb/hour 38.7 tons/year
Synthetically Limited? [x ] Yes [ ] No
Range of Estimated Fugitive/Other Emissions:
[ ] 1 [ ] 2 [ ] 3 to tons/yr
5. Emission Factor: 0.05 %s
Reference: AP-42 and %S
7. Emissions Method Code:
[x]0 []1 []2 []3 []4 []5
3. Calculation of Emissions (limit to 600 characters):
1,449 gal/hr x 7.2 lb/gal x 0.0005 lb S/lb fuel x 2 lb SO2/lb S = 10.43 lbs/hr
P. Pollutant Potential/Estimated Emissions Comment (limit to 200 characters):
Annual SO2 emissions from #2 fuel oil firing for all 3 boilers shall not exceed 25 TPY, except during periods of natural gas unavailability, emissions shall not exceed 40 TPY with proper notification.

### Emissions Unit Information Section 3 of 3 Allowable Emissions (Pollutant identified on front page)

1.	Basis for Allowable Emissions Code:
	OTHER

- 2. Future Effective Date of Allowable Emissions:
- 3. Requested Allowable Emissions and Units:

0.05 % Sulfur

4. Equivalent Allowable Emissions:

10.43 lb/hour

38.7 tons/year

5. Method of Compliance (limit to 60 characters):

Fuel Oil analysis

6. Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode) (limit to 200 characters):

See Attachment SCC-EU1-HA6. Maximum annual emissions under normal operations, when natural gas is available is 25 TPY. Emissions under natural gas curtailment cannot exceed 40 TPY.

B.

**A.** .

- 1. Basis for Allowable Emissions Code:
- 2. Future Effective Date of Allowable Emissions:
- 3. Requested Allowable Emissions and Units:
- 4. Equivalent Allowable Emissions:

lb/hour

tons/year

- 5. Method of Compliance (limit to 60 characters):
- 6. Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode) (limit to 200 characters):

Emissions	Unit In	formation	Section	3	of	3

### H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

### **Pollutant Detail Information**:

1. Pollutant Emitted: NOx				
2. Total Percent Efficiency of Control: %				
3. Potential Emissions: 34.94 lb/hour 153.1 tons/year				
4. Synthetically Limited? [ ] Yes [x] No				
5. Range of Estimated Fugitive/Other Emissions:				
[ ] 1				
6. Emission Factor: 0.2 Ib/MMBtu				
Reference: Proposed Limit				
7. Emissions Method Code:				
[x]0 []1 []2 []3 []4 []5				
8. Calculation of Emissions (limit to 600 characters):				
NOx emissions capped at current permit limit. Equivalent to 0.1625 lb/MMBtu at max heat input.				
· · · · · · · · · · · · · · · · · · ·				
9. Pollutant Potential/Estimated Emissions Comment (limit to 200 characters):				
The maximum allowable NOx emissions shall not exceed 0.2 lb/MMBtu, 34.94 lbs/hr and 153.1 TPY per boiler. Total NOx emissions from all three boilers limited to 310 TPY.				

### Emissions Unit Information Section 3 of 3 Allowable Emissions (Pollutant identified on front page)

A.

1.	Basis for Allowable Emissions Code:  OTHER
2.	Future Effective Date of Allowable Emissions:
3.	Requested Allowable Emissions and Units  0.2 lb/MMBtu
4.	Equivalent Allowable Emissions: 34.94 lb/hour 153.1 tons/year
5.	Method of Compliance (limit to 60 characters):  CEM for NOx
6.	Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode) (limit to 200 characters):
	Self-imposed limit by permittee. Based on natural gas firing.
В.	
1.	Basis for Allowable Emissions Code:
2.	Future Effective Date of Allowable Emissions:
3.	Requested Allowable Emissions and Units:
4.	Equivalent Allowable Emissions: lb/hour tons/year
5	Method of Compliance (limit to 60 characters)

6. Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode)

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(limit to 200 characters):

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#### H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information**:

1. Pollutant Emitted: PM
2. Total Percent Efficiency of Control %
3. Potential Emissions: 2.9 lb/hour 11.5 tons/year
4. Synthetically Limited? [ x ] Yes [ ] No
5. Range of Estimated Fugitive/Other Emissions.
[ ] 1  [ ] 2  [ ] 3 totons/yr
6. Emission Factor: 2 lbs/1000 gal
Reference: AP-42
7. Emissions Method Code:
[ ]0  [ ]1  [ ]2  [ <b>x</b> ]3  [ ]4  [ ]5
8. Calculation of Emissions (limit to 600 characters):
Fuel Oil: 1,449.3 gal/hr x 2 lbs/1000 gal = 2.90 lb/hr
9. Pollutant Potential/Estimated Emissions Comment (limit to 200 characters):
See Attachment A for additional calculations

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1.	Basis for Allowable Emissions Code:		
2.	Future Effective Date of Allowable Emissions:		
3.	Requested Allowable Emissions and Units:		
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 characters):		
6.	Pollutant Allowable Emissions Comment (Desc. (limit to 200 characters):	of Related Operating	g Method/Mode)
			•
В.			
1.	Basis for Allowable Emissions Code:		
2.	Future Effective Date of Allowable Emissions:		
3.	Requested Allowable Emissions and Units:		
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 characters):		
6.	Pollutant Allowable Emissions Comment (Desc.	of Related Operating	g Method/Mode)

(limit to 200 characters):

<b>Emissions</b>	Unit	Information	Section	3	of	3

## H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information**:

1. Pollutant Emitted: PM10
2. Total Percent Efficiency of Control: %
3. Potential Emissions: 1.45 lb/hour 6.1 tons/year
4. Synthetically Limited? [x] Yes [] No
5. Range of Estimated Fugitive/Other Emissions:
[ ] 1 [ ] 2 [ ] 3 to tons/yr
6. Emission Factor: 50 % of PM
Reference: AP-42
7. Emissions Method Code:
[ ]0
8. Calculation of Emissions (limit to 600 characters):
Fuel Oil: 2.90 lb/hr x 0.5 = 1.45 lb/hr
· 
9. Pollutant Potential/Estimated Emissions Comment (limit to 200 characters):
See Attachment A for additional calculations
·

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Emissions Unit Informa	tion Section 3	of3	
Allowable Emissions (P	ollutant identified	on front page)	

Α.	
1.	Basis for Allowable Emissions Code:
2.	Future Effective Date of Allowable Emissions:
3.	Requested Allowable Emissions and Units:
4.	Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance (limit to 60 characters):
6.	Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode) (limit to 200 characters):
<u>В</u> .	
1.	Basis for Allowable Emissions Code:
2.	Future Effective Date of Allowable Emissions:
3.	Requested Allowable Emissions and Units:
4.	Equivalent Allowable Emissions: lb/hour tons/year
5.	Method of Compliance (limit to 60 characters):
6.	Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode) (limit to 200 characters):

<b>Emissions</b>	Unit	Information	Section	3	of	3
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# H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION (Regulated Emissions Units Only - Emissions Limited Pollutants Only)

#### **Pollutant Detail Information**:

1. Pollutant Emitted: CO	
2. Total Percent Efficiency of Control:	%
3. Potential Emissions: 8.96 lb/hour	19 tons/year
4. Synthetically Limited? [ ] Yes [x] No	
5. Range of Estimated Fugitive/Other Emissions:	
[ ]1 [ ]2 [ ]3to	tons/yr
6. Emission Factor: 50 ppmvd	
Reference: Test Data	
7. Emissions Method Code:	
[.]0 [x]1 []2 []3 [	]4 [ ]5
8. Calculation of Emissions (limit to 600 characters):	
Natural Gas: 41,084 dscfm x 50 ppmvd x 60 min/hr x 2, R/ft-lb x 1/528 deg. R = 8.96 lb/hr	116.8 lb/sq.ft. x (28/1545) lb-deg.
• .	
	· · ·
9. Pollutant Potential/Estimated Emissions Comment (limi	
Annual emissions based on 25 ppmvd. See Attachment A.	
·	

	ssions Unit Information Section <u>3</u> of _ wable Emissions (Pollutant identified on front	page)	•
۱.			
1.	Basis for Allowable Emissions Code		
2.	Future Effective Date of Allowable Emissions:		
3.	Requested Allowable Emissions and Units:		
4.	Equivalent Allowable Emissions:	lb/hour	tons/year
5.	Method of Compliance (limit to 60 characters):		-
ι.	Poliutant Allowable Emissions Comment (Desc.	of Related Oper	ating Method/Mode)
·.	Pollutant Allowable Emissions Comment (Desc. (limit to 200 characters):	of Related Oper	ating Method/Mode)
	•	of Related Oper	ating Method/Mode)
	•	of Related Oper	ating Method/Mode)
	(limit to 200 characters):	of Related Oper	ating Method/Mode)
	(limit to 200 characters):  Basis for Allowable Emissions Code:	of Related Oper	ating Method/Mode)
2.	Basis for Allowable Emissions Code:  Future Effective Date of Allowable Emissions:	lb/hour	tons/year

Emissions und information section • of •	Emissions	Unit Information	Section	3	of	3
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### I. VISIBLE EMISSIONS INFORMATION (Regulated Emissions Units Only)

<u>Visible</u>	Emissions Limitations Visible Emissions Limitation 1 of 2
1.	Visible Emissions Subtype: VE05
2.	Basis for Allowable Opacity: [x ] Rule [ ] Other
	Requested Allowable Opacity Normal Conditions: 5 % Exceptional Conditions: % Maximum Period of Excess Opacity Allowed: min/hour
4.	Method of Compliance: EPA Method 9
5.	Visible Emissions Comment (limit to 200 characters):  Natural gas firing; based on BACT
<u>Visible</u>	Emissions Limitations: Visible Emissions Limitation 2 of 2
1.	Visible Emissions Subtype: VE10
2.	Basis for Allowable Opacity: [x] Rule [] Other
	Requested Allowable Opacity Normal Conditions: 10 % Exceptional Conditions: % Maximum Period of Excess Opacity Allowed: min/hour
4.	Method of Compliance: EPA Metod 9
5.	Visible Emissions Comment (limit to 200 characters):  No. 2 fuel oil firing; based on BACT.

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Emissions Unit	Information Section	3	of	3

# J. CONTINUOUS MONITOR INFORMATION (Regulated Emissions Units Only)

1.	Parameter Code: EM	2. Pollutant(s):	NOx
3.	CMS Requirement: [x ] Rule [ ]	Other	
4.	Monitor Information: Monitor Manufacturer: Servomex Model Number: 1491	Serial Number: 103	3
5.	Installation Date: 01 Feb 1994		
6.	Performance Specification Test Date:	21 Jun 1994	_
7.	Continuous Monitor Comment (limit to	200 characters):	
	CEMS for nitrogen oxides shall be operequirements of 40 CFR 60.48b.	erated and maintained in a	ccordance with
	•		
ont		us Monitor of	
<u>ont</u>	inuous Monitoring System Continuou	as Monitor of 2. Pollutant(s):	_
1.	inuous Monitoring System Continuou  Parameter Code:		
1.	inuous Monitoring System Continuou  Parameter Code:  CMS Requirement: [ ] Rule [ ]  Monitor Information:	2. Pollutant(s):	
1.	inuous Monitoring System Continuou  Parameter Code:  CMS Requirement: [ ] Rule [ ]	2. Pollutant(s):	
1.	inuous Monitoring System Continuous  Parameter Code:  CMS Requirement: [ ] Rule [ ]  Monitor Information: Monitor Manufacturer:	2. Pollutant(s): Other	
1. 3. 4.	inuous Monitoring System Continuous  Parameter Code:  CMS Requirement: [ ] Rule [ ]  Monitor Information:  Monitor Manufacturer:  Model Number:  Installation Date:	2. Pollutant(s): Other	

Emissions Unit Information Section 3 of 3	
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# K. PREVENTION OF SIGNIFICANT DETERIORATION (PSD) INCREMENT TRACKING INFORMATION

(Regulated and Unregulated Emissions Units)

#### **PSD Increment Consumption Determination**

1. Increment Consuming for Particulate Matter or Sulfur Dioxide?

If the emissions unit addressed in this section emits particulate matter or sulfur dioxide, answer the following series of questions to make a preliminary determination as to whether or not the emissions unit consumes PSD increment for particulate matter or sulfur dioxide. Check the first statement, if any, that applies and skip remaining statements.

- The emissions unit is undergoing PSD review as part of this application, or has [x] undergone PSD review previously, for particulate matter or sulfur dioxide. If so, emissions unit consumes increment. The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after January 6, 1975. If so, baseline emissions are zero, and the emissions unit consumes increment. The facility addressed in this application is classified as an EPA major source and ſ the emissions unit began initial operation after January 6, 1975, but before December 27, 1977. If so, baseline emissions are zero, and the emissions unit consumes increment. For any facility, the emissions unit began (or will begin) initial operation after December 27, 1977. If so, baseline emissions are zero, and emissions unit consumes increment
- None of the above apply. If so, the baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

2. Increment Consuming for Nitrogen Dioxide?

If the emissions unit addressed in this section emits nitrogen oxides, answer the following series of questions to make a preliminary determination as to whether or not the emissions unit consumes PSD increment for nitrogen dioxide. Check first statement, if any, that applies and skip remaining statements.

- The emissions unit addressed in this section is undergoing PSD review as part of this application, or has undergone PSD review previously, for nitrogen dioxide. If so, emissions unit consumes increment.
- The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after February 8, 1988. If so, baseline emissions are zero, and the source consumes increment.
- The facility addressed in this application is classified as an EPA major source and the emissions unit began initial operation after February 8, 1988, but before March 28, 1988. If so, baseline emissions are zero, and the source consumes increment.
- For any facility, the emissions unit began (or will begin) initial operation after March 28, 1988. If so, baseline emissions are zero, and the emissions unit consumes increment.
- None of the above apply. If so, baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

3.	Increment Consuming/Exp PM SO <sub>2</sub> NO <sub>2</sub>	panding Code:  [x ] C  [x ] C  [x ] C	[ ]	] E ] E ] E	[ ] Unknown [ ] Unknown [ ] Unknown
4.	Baseline Emissions: PM SO <sub>2</sub> NO <sub>2</sub>	lb/hour lb/hour			tons/year tons/year tons/year
5.	PSD Comment (limit to 20	00 characters):			

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### L. EMISSIONS UNIT SUPPLEMENTAL INFORMATION (Regulated Emissions Units Only)

### Supplemental Requirements for All Applications

, 1.	Process Flow Diagram	
-	[ x ] Attached, Document ID:       SCC-EU1-L1         [ ] Not Applicable       [ ] Waiver Requested	
2.	Fuel Analysis or Specification	
	[ x ] Attached, Document ID: SCC-EU1-L2         [ ] Not Applicable       [ ] Waiver Requested	
3.	Detailed Description of Control Equipment	
	[ ] Attached, Document ID:	
4.	Description of Stack Sampling Facilities	
	[ ] Attached, Document ID:	
5.	Compliance Test Report	
	[ ] Attached, Document ID: [x ] Not Applicable [ ] Previously Submitted, Date:	
6.	Procedures for Startup and Shutdown	
	[ ] Attached, Document ID: [x ] Not Applicable	
7.	Operation and Maintenance Plan	
	[ ] Attached, Document ID: [x ] Not Applicable	
8.	Supplemental Information for Construction Permit Application	
	[X] Attached, Document ID: Attachment A [ ] Not Applicable	
9.	Other Information Required by Rule or Statute	
	[ ] Attached, Document ID: [X] Not Applicable	

<b>Emissions Unit Information Section</b>	3	of <sup>3</sup>	
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### Additional Supplemental Requirements for Category I Applications Only

10.	Al	tern	ative Methods of Operation
	[	]	Attached, Document ID: [ ] Not Applicable
11.	Al	tern	ative Modes of Operation (Emissions Trading)
	[	]	Attached, Document ID: [ ] Not Applicable
12.	Id	enti	fication of Additional Applicable Requirements
	[	]	Attached, Document ID: [ ] Not Applicable
13.	Co	omp	liance Assurance Monitoring Plan
	[	]	Attached, Document ID: [ ] Not Applicable
14.	A	cid I	Rain Permit Application (Hard Copy Required)
	[	]	Acid Rain Part - Phase II (Form No. 62-210.900(1)(a)) Attached, Document ID:
	[	]	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.) Attached, Document ID:
	[	]	New Unit Exemption (Form No. 62-210.900(1)(a)2.) Attached, Document ID:
	[	]	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.) Attached, Document ID:
÷	[	]	Not Applicable

# ATTACHMENT A PSD REPORT

# ATTACHMENT A PSD REPORT

#### 1.0 INTRODUCTION

Stone Container Corporation (SCC) currently operates a 100-percent recycled fiber paper mill facility located in Jacksonville, Florida. The facility has been operating as a 100-percent recycled fiber facility since 1992. Formerly, the facility had two bark boilers and three power boilers to provide steam to the paper making process. These five boilers were shutdown in March, 1994, when the U.S. Generating Company Cedar Bay facility began commercial operation.

The Cedar Bay cogeneration facility, licensed under the Florida Power Plant Site Certification Act (FPPSCA), is located adjacent to the existing SCC facility. This coal-fired power plant provides part of the steam required for the recycle fiber facility. The recycle fiber facility requires additional steam beyond that provided by the Cedar Bay facility. As a result, three new package boilers were installed by SCC to provide this necessary steam. These package boilers are fueled with natural gas and very low sulfur fuel oil. A federal and state PSD construction permit for the three package boilers was issued in July, 1993 (AC16-222359; PSD-FL-198). These permits were amended in 1995 to allow increased steam production, i.e., 125,000 lb/hr steam for each of the three package boilers (see Appendix A).

SCC is currently requesting an increase in the maximum steam production rate for each boiler from 125,000 lb/hr to 150,000 lb/hr steam. More flexibility in steam production is desired by SCC in the case of a shutdown or curtailment by Cedar Bay. Although at present SCC anticipates that this increased level of steam production will be needed infrequently, such as during a scheduled outage by Cedar Bay, SCC would like to plan for the future independently of Cedar Bay.

Although the increase in the maximum steam rates of the three boilers will result not result in an increase in allowable emissions for the boilers, an increase in actual air emissions will occur. The requested revisions for the package boilers will constitute a major modification at a major stationary facility under current federal and Florida PSD regulations. This report addresses the requirements of the PSD review procedures, pursuant to rules and regulations implementing the Clean Air Act (CAA) Amendments of 1977.

This application contains six additional sections. A complete description of the project, including air emission rates, is presented in Section 2.0. The air quality requirements for the project and new source review applicability are discussed in Section 3.0. A preconstruction ambient air quality data analysis is presented in Section 4.0. The control technology review and best available control technology (BACT) analysis is presented in Section 5.0. The required air quality impact analysis is presented in Section 6.0, and an additional impact analysis (i.e., to soils, vegetation and visibility) is described in Section 7.0.

#### 2.0 PROJECT DESCRIPTION

#### 2.1 GENERAL

SCC currently operates a 100 percent recycled fiber paper mill located in Jacksonville, Florida (see Attachment SCC-FE-1). Three package boilers are operated to support the paper mill operations. The boilers are fired with natural gas or very low sulfur No. 2 fuel oil with a maximum sulfur content of 0.05 percent. The current maximum steam production for each boiler is 125,000 lb/hr steam. The current maximum heat input to each boiler is 174.7 MMBtu/hr when firing natural gas, and 164.5 MMBtu/hr when firing fuel oil.

The Cedar Bay cogeneration facility currently supplies SCC with steam. However, the SCC recycle fiber facility at times requires additional steam beyond that provided by the Cedar Bay facility. SCC would like to plan for future operation and maximum flexibility by permitting the boilers to operate up to 150,000 lb/hr steam each. Although SCC anticipates that operation at this level with all three boilers will be very infrequent, SCC will no longer be constrained by Cedar Bay operation.

SCC is proposing to increase the maximum steam rate and heat input rate to the boilers, while maintaining the current permitted emission levels. The boilers currently have permitted allowable emissions rates for nitrogen oxides (NO<sub>x</sub>) and sulfur dioxide (SO2). Each of the three package boilers will be rated at 150,000 lb/hr steam at 650 psig and 750°F. Maximum heat input to each boiler will be 215 MMBtu/hr when firing natural gas, and 200 MMBtu/hr when firing No. 2 fuel oil. Design parameters for each package boiler at the increased steam production rate are presented in Table 2-1.

Firing of No. 2 fuel oil will be limited to 10,750,000 gallons per year for all three boilers combined. This limit will insure SO<sub>2</sub> emissions do not exceed 40 tons per year.

#### 2.2 EMISSIONS OF REGULATED POLLUTANTS

The package boilers are subject to the federal New Source Performance Standards (NSPS) for industrial boilers since the maximum heat input to each boiler is greater than 100 MMBtu/hr. The NSPS are contained in the Code of Federal Regulations (CFR), Title 40, Part 60, Subpart Db, and are summarized in Table 2-2. The NSPS limit emissions of NO, to 0.2 lb/MMBtu for both natural

gas firing and distillate fuel oil firing in high heat release rate boilers. The NSPS defines a high heat release rate boiler as a boiler heat release rate of greater than 70,000 Btu/hr-ft<sup>3</sup>.

SO<sub>2</sub> emissions are limited under the NSPS to 0.50 lb/MMBtu(equivalent to 0.5 percent sulfur fuel) for sources which do not use an add-on SO<sub>2</sub> control device, such as a flue gas desulfurization system. The No. 2 fuel oil burned in the package boilers contains 0.05 percent sulfur (0.05 lb/MMBtu) or less, which will meet the NSPS requirements. There is no PM limit under NSPS for natural gas or distillate fuel oil firing.

The maximum estimated hourly emissions of regulated pollutants from each of the package boilers are presented in Table 2-3. Emissions for both No. 2 fuel oil and natural gas are shown. Also shown is the equivalent emission rate in terms of lb/MMBtu heat input.

For No. 2 fuel oil firing, total suspended particulate matter [PM(TSP)] emissions and emissions of particulate matter with an aerodynamic particle size diameter of 10 micrometers ( $\mu$ m) or less (PM10) are based on EPA Publication AP-42 factors for uncontrolled oil-fired boilers. The AP-42 data show that 50 percent of the PM(TSP) emissions are of PM10 size (refer to Appendix B).

The fuel oil burned in the package boilers will be a No. 2 fuel oil with a maximum sulfur content of 0.05 percent, equivalent to 0.052 lb/MMBtu, to meet the NSPS. Natural gas contains only trace quantities of sulfur.

SCC is retaining the current hourly and annual NOx emission rate for each boiler of 39.94 lb/hr and 153.1 TPY. Thus, at the maximum heat input rate, equivalent emissions will be limited to 0.1747 lb/MMBtu for oil firing, and to 0.1625 lb/MMBtu for natural gas firing. At lower loads, the boilers will continue to meet a limit of 0.2 lb/MMBtu, which is equivalent to federal NSPS for new boilers of greater than 100 MMBtu/hr heat input capacity with a high heat release rate and firing distillate oil or natural gas. The design heat release rate of the boilers will be 119,474 Btu/hr-ft³ for No. 2 fuel oil and 128,435 Btu/hr-ft³ for natural gas, which classifies the boilers as high heat release rate boilers.

Emissions of VOC from the boilers are based on AP-42 factors for distillate-oil-fired and natural gas-fired boilers (see Appendix B). Maximum hourly carbon monoxide (CO) emissions for both

No. 2 distillate oil firing and natural gas firing are based upon a maximum CO concentration of 50 ppm in the exhaust gases, based upon source testing of the boilers. The equivalent hourly CO emission rate is 0.0432 lb/MMBtu for oil firing, and 0.0417 lb/MMBtu for gas firing. Maximum annual CO emissions are based upon one-half of the hourly rate, or 25 ppmvd, also based on source test data.

Emissions of other PSD regulated pollutants are based on published emission factors, as indicated in the footnotes to Table 2-3. As shown in the table, fuel oil burning in the package boilers results in the maximum emissions for all pollutants on a lb/MMBtu basis.

Maximum estimated annual emissions for all three package boilers combined are presented in Table 2-4. The maximum annual emissions for certain pollutants are limited based on total annual fuel oil firing equivalent to  $1.4835 \times 10^{12}$  Btu/yr (equivalent to 10,750,000 gal/yr). This limitation ensures that the maximum annual  $SO_2$  emission due to all three boilers does not exceed 40 tons per year (TPY). There is no restriction on annual natural gas firing in the boilers.

Presented in Table 2-5 are the maximum annual emissions on a per boiler basis. The maximum emissions for each boiler take into consideration the total fuel oil burning limitation of 10,750,000 gal/yr for all three boilers.

#### 2.3 STACK PARAMETERS

Stack parameters for the package boilers are presented in Table 2-1. All three boilers are served by a single common stack 200 feet (ft) tall with an 8.0 ft diameter. The exhaust gases from each are ducted to this common stack. The location of the common stack in relation to the structures at SCC is shown in Attachment SCC-FE-2.

Table 2-1. Design Parameters for New Package Boilers

Parameter	Units	No. 2 Fuel Oil (per boiler)	Natural Gas (per boiler)
Steam Flow	lb/hr	150,000	150,000
Steam Pressure	psi	650	650
Steam Temperature	deg. F	709	750
Heat Input	MMBtu/hr	200	215
Furnace Volume	ft^3	1,674	1,674
Heat Release Rate	Btu/hr-ft^3	119,474	128,435
Fuel Heating Value	Btu/gal	138,000	
	Btu/lb	19,167 (a)	
	Btu/scf		1,000
Fuel Flow	lb/hr	10,435	
	gal/hr	1,449.3	
	scf/hr		215,000
Exhaust Gas:			
Temperature	deg. F	345	330
Moisture	%	10	10
Flow Rate	lb/hr	192,000	199,000
	acfm	67,149	68,300
	dscfm	39,638	41,084
Common Stack (b)			
Diameter	ft	8	8
Velocity	ft/s	66.79	67.94
Height	ft	200	200

<sup>(</sup>a) Density of No. 2 fuel oil is approximately 7.2 lb/gal.

<sup>(</sup>b) All three boilers will exhaust into a common stack. Velocity shown is total all three boilers.

Table 2-2. NSPS for Natural Gas/Oil-Fired Steam-Generating Units With Heat Input Between 100 x 106 and 250 x 106 Btu/hr

Pollutant	Fuel	Annual Capacity Factor (%)	Standard
SO <sub>2</sub>	Fuel oil	31-100 on oil	0.80 lb/10 <sup>6</sup> Btu; 90% reduction <sup>a</sup>
	Fuel oil	0-30 on oil	0.50 lb/106 Btu
	Natural gas	0-100 on gas	No SO <sub>2</sub> limit
PM	Fuel oil	0-100	<ul> <li>a. 0.10 lb/10<sup>6</sup> Btu if a conventional or emerging SO<sub>2</sub> control technology is used</li> <li>b. no PM limit if an SO<sub>2</sub> control technology is not used</li> </ul>
	Natural gas	0-100	No PM limit
Opacity	Fuel oil or natural gas	0-100	20% opacity, except 27% for one 6-minute period per hour
NO <sub>x</sub>	Distillate oil or natural gas	11-100 on oil or gas	Distillate oil or natural gas  a. Low heat release rate 0.10 lb/10 <sup>6</sup> Btu  b. High heat release rate 0.20 lb/10 <sup>6</sup> Btu
	Distillate oil	0-10 on oil	No NO <sub>x</sub> standard

Note:  $1b/10^6$  Btu = pounds per million British thermal units.  $NO_x = \text{nitrogen oxides}.$   $SO_2 = \text{sulfur dioxide}.$ 

Source: 40 CFR 60, Subpart Db.

 $<sup>^{\</sup>circ}$  Percentage reduction requirement does not apply if burning very-low-sulfur oil (<0.50 lb/10 $^{\circ}$  Btu).

Table 2-3. Maximum Hourly Emissions from Modified Package Boilers (per boiler), Stone Container Corporation, Jacksonville Mill

	N	o. 2 Fuel	Oil			ı	Natural G	as		
Regulated			Hourly	Hourly Emissions	Equivalent			Hourty	Hourly Emissions	Equivaler
Pollutant	Emission Factor (a)	Ref.	Activity Factor (a)	(lbs/hr)	(ib/MMBtu)	Emission Factor (b)	Ref.	Activity Factor (b)	(lbs/hr)	(Ib/MMBtu
Criteria and Precursor Pollutar	nts									
Particulate Matter (PM)	2 lbs/1000 gal	1	1,449.3 gal/hr	2.90	0.0145	5 lb/MMscf .	· 1	0.215 MMscf/hr	1.08	0.0050
Particulate Matter (PM10)	50% of PM	1	1,449.3 gai/hr	1.45	0.0072	5 lb/MMscf	1	0.215 MMscf/hr	1.08	0.0050
Sulfur dioxide	7.2 lbs/1000 gal	2	1,449.3 gal/hr	10.43	0.052	0.6 lb/MMscf	1	0.215 MMscf/hr	0.13	0.0006
Nitrogen oxides	0.2 lbs/MMBtu	3	200 MMBtu/hr	34.94	0.2	0.2 lbs/MMBtu	3	215 MMBtu/hr	34.94	0.2
Carbon monoxide	50 ppmvd	4	39,638 dscfm	8.64	0.0432	50 ppmvd	4	41,084 dscfm	8.96	0.0417
voc	0.2 lbs/1000 gal	1	1,449.3 gal/hr	0.29	0.0014	1.4 lbs/MMscf	1	0.215 MMscf/hr	0.30	0.0014
Lead - Total	8.9E-06 lbs/MMBtu	1	200 MMBtu/hr	0.0018	8.90E-06	2.71E-04 lbs/MMscf	1	0.215 MMscf/hr	5.8E-05	2.7E-07
Designated Pollutants										
Sulfuric Acid Mist	0.12 lbs/1000 gal	5	1,449.3 gal/hr	0.18	8.88E-04			-		
Fluorides - Total	3.2E-05 lbs/MMBtu	6	200 MMBtu/hr	0.0064	3.20E-05	-		-	-	
Hazardous Air Pollutants										
Beryllium	2.5E-06 lbs/MMBtu	1	200 MMBtu/hr	5.0E-04	2.50E-06				-	
Mercury	3.0E-06 lbs/MMBtu	1	200 MMBtu/hr	0.00060	3.00E-06	1.5E-10 lbs/MMBtu	7	215 MMBtu/hr	3.2E-08	1.50E-10

#### Footnotes:

- (a) Based on firing only No. 2 fuel oil (0.05% Sulfur) at 200 MMBtu/hr; No. 2 oil @ 138,000 Btu/gal and 7,2 lb/gal.
- (b) Based on firing only natural gas at 215 MMBtu/hr; 1,000 Btu/scf.

#### References

- 1. Based on Compilation of Air Pollutant Emission Factors, AP-42, Tables 1.3-1, 1.3-2, 1.3-5, 1.3-9, 1.4-1, 1.4-2, 1.4-3 and 1.4-5.
- 2. 7.2 lb/gal x 0.0005 lbS/lb fuel x 2 lb SO2/lb fuel x 1000 gal= 7.2 lb/1000 gal
- 3. Proposed by permittee; current permit limits.
- 4. Based on test data from Stone Container package boilers which showed maximum hourly CO emissions of less than 50 ppmvd.
- 5. AP-42, Table 1.3-2. Factor is the SO3 emission factor of 2S lb/1000 gal, where S= fuel sulfur content, multiplied by the ratio of H2SO4 to SO3.
- 6. Emissions Assessment of Conventional Stationary Combustion Sources: Vol. V.:
- Industrial Combustion Sources-Uncontrolled Fuel Oil Combustion (EPA-600/7-81-003c), Table 18.
- 7. From "Study of Hazardous Air Pollutant Emissions From Electric Utility Steam Generating Units", Report to Congress, 1997.

Table 2-4. Maximum Annual Emissions From Modified Package Boilers (total all boilers), Stone Container Corporation

		No. 2 Fuel Oil			Natural Gas		Total
Regulated		Annual	Annual Emissions		Annual	Annual Emissions	Annual Emissions
Pollutant	Emission Factor (a)	Activity Factor (b)	(TPY)	Emission Factor (a)	Activity Factor (b)	(TPY)	(TPY)
1 Onatant	200.0 40.0 (4)	richtrity i deter (b)		Emiliation (a)	/ tolivily i dolor (b)	(11.1)	
riteria and Precursor Polluta	ints			•	·.		
articulate Matter (PM)	0.0145 lb/MMBtu	1,483,500 MMBtu/yr	10.76	0.0050 lb/MMBtu	4,055,438 MMBtu/yr	10.14	20.89
Particulate Matter (PM10)	0.0072 lb/MMBtu	1,483,500 MMBtu/yr	5.34	0.0050 lb/MMBtu	4,055,438 MMBtu/yr	10.14	15.48
Sulfur dioxide	0.052 lb/MMBtu	1,483,500 MMBtu/yr	38.6	0.0006 lb/MMBtu	4,055,438 MMBtu/yr	1.22	39.79
litrogen oxides	0.2 lb/MMBtu	1,483,500 MMBtu/yr	(c)	0.2 lb/MMBtu	4,055,438 MMBtu/yr	(c)	310 (
Carbon monoxide	0.0216 lb/MMBtu	1,483,500 MMBtu/yr	16.02	0.0209 lb/MMBtu	4,055,438 MMBtu/yr	42.38	58.4
oc	0.0014 lb/MMBtu	1,483,500 MMBtu/yr	1.04	0.0014 lb/MMBtu	4,055,438 MMBtu/yr	2.84	3.88
ead - Total	8.90E-06 lb/MMBtu	1,483,500 MMBtu/yr	0.0066	2.71E-07 lb/MMBtu	4,055,438 MMBtu/yr	0.00055	0.0072
esignated Pollutants		•	•				
ulfuric Acid Mist	8.88E-04 lbs/MMBtu	1,483,500 MMBtu/yr	0.66		_		0.66
luorides - Total	3.20E-05 lbs/MMBtu	1,483,500 MMBtu/yr	0.024		-		0.024
azardous Air Pollutants							
eryllium	2.50E-06 lbs/MMBtu	1,483,500 MMBtu/yr	0.00185				0.00185
fercury	3.00E-06 lbs/MMBtu	1,483,500 MMBtu/yr	0.0022	1.50E-10 lbs/MMBtu	4,055,438 MMBtu/yr	3.0E-07	0.0022

#### Footnotes

- (a) Obtained from Table 2-3, except for CO. For CO, annual emissions are based on 25 ppm, or one-half of maximum hourly emissions.
- (b) Based on maximum amount of fuel oil firing in order not to exceed 40 TPY SO2 emissions cap, with remainder of fuel firing due to natural gas. The maximum total heat input due to fuel oil firing is equivalent to 10,750,000 gal/yr fuel oil at 138,000 Btu/gal. This is equivalent to one boiler operating at 100% capacity on fuel oil for 7,417 hr/yr.
- (c) Total NOx emissions capped at 310 TPY for facility.

Table 2-5. Maximum Annual Emissions from Each Modified Package Boilers (per boiler), Stone Container Corporation, Jacksonville Mill

		No. 2 Fuel Oil			Natural Gas		Total
Regulated Pollutant	Emission Factor (a)	Annual Activity Factor (b)	Annual Emissions (TPY)	Emission Factor (a)	Annual Activity Factor (b)	Annual Emissions (TPY)	Annual Emissions (TPY)
Criteria and Precursor Polluta	ints				*		
Particulate Matter (PM)	0.0145 lb/MMBtu	1,483,500 MMBtu/yr	10.76	0.0050 lb/MMBtu	288,745 MMBtu/yr	0.72	11.48
Particulate Matter (PM10)	0.0072 lb/MMBtu	1,483,500 MMBtu/yr	5.34	0.0050 lb/MMBtu	288,745 MMBtu/yr	0.72	6.06
sulfur dioxide	0.052 lb/MMBtu	1,483,500 MMBtu/yr	38.57	0.0006 lb/MMBtu	288,745 MMBtu/yr	0.09	38.66
itrogen oxides	0.2 lb/MMBtu	1,483,500 MMBtu/yr	(c)	0.2 lb/MMBtu	1,883,400 MMBtu/yr	(c)	153.1 (
arbon monoxide	0.0216 lb/MMBtu	1,483,500 MMBtu/yr	16.02	0.0209 lb/MMBtu	288,745 MMBtu/yr	3.02	19.0
oc	0.0014 lb/MMBtu	1,483,500 MMBtu/yr	1:04	0.0014 lb/MMBtu	288,745 MMBtu/yr	0.20	1.24
ead - Total	8.90E-06 lb/MMBtu	1,483,500 MMBtu/yr	0.0066	2.7E-07 lb/MMBtu	288,745 MMBtu/yr	3.9E-05	0.0066
esignated Pollutants							
ulfuric Acid Mist	8.88E-04 lbs/MMBtu	1,483,500 MMBtu/yr	0.66		-		0.66
luorides - Total	3.20E-05 lbs/MMBtu	1,483,500 MMBtu/yr	0.024				0.024
azardous Air Pollutants							
eryllium	2.50E-06 lbs/MMBtu	1,483,500 MMBtu/yr	0.0019	· <b>-</b>			0.0019
Mercury	3.00E-06 lbs/MMBtu	1,483,500 MMBtu/yr	0.0022	1.5E-10 lbs/MMBtu	288,745 MMBtu/yr	2.2E-08	0.0022

#### Footnotes

<sup>(</sup>a) Obtained from Table 2-3, except for CO. For CO, annual emissions are based on 25 ppm, or one half of maximum hourly emissions.

<sup>(</sup>b) Based on maximum amount of fuel oil firing in order to not exceed 40 TPY SO2 emission cap, with remainder of fuel fining due to natural gas. The maximum total heat input due to fuel oil firing is equivalent to 10,750,000 gal/yr of fuel oil at 138,000 Btu/gal. This is equivalent to one boiler operating for 7,417 hr/yr on fuel oil.

<sup>(</sup>c) Total NOx emissions capped at 153.1 TPY for each boiler.

# 3.0 PSD SOURCE APPLICABILITY ANALYSIS

Federal PSD requirements are contained in Title 40, Code of Federal Regulations (CFR), Part 52.21, Prevention of Significant Deterioration of Air Quality. The State of Florida has adopted PSD regulations (Chapter 62-212.400, F.A.C.) that essentially are identical to the federal regulations. PSD regulations require that all new major stationary sources or major modifications to existing major sources of air pollutants regulated under CAA be reviewed and a construction permit issued. Florida's State Implementation Plan (SIP), which contains PSD regulations, has been approved by EPA and PSD approval authority in Florida has been granted to FDEP.

A "major facility" is defined under Florida PSD regulations as any one of 28 named source categories that has the potential to emit 100 tons per year (TPY) or more of any pollutant regulated under the CAA, or any other stationary facility that has the potential to emit 250 TPY or more of any pollutant regulated under CAA. A "source" is defined as an identifiable piece of process equipment or emissions unit. "Potential to emit" means the capability, at maximum design capacity, to emit a pollutant, considering the application of control equipment and any other federally enforceable limitations on the source's capacity. A "major modification" is defined under PSD regulations as a change at an existing major stationary facility that increases emissions by greater than significant amounts. PSD significant emission rates are shown in Table 3-1.

The SCC facility is located in Duval County, which has been designated by EPA and FDEP as an attainment area for SO<sub>2</sub> and NO<sub>x</sub>. Duval County and surrounding counties are designated as PSD Class II areas for SO<sub>2</sub> and NO<sub>x</sub>. The site is located about 61 km from a PSD Class I area (Okefenokee National Wilderness Area).

The SCC facility is an existing major stationary facility because potential emissions of certain regulated pollutants exceed 100 TPY (for example, potential NO<sub>x</sub> emissions currently exceeds 100 TPY). SCC has previously been issued a PSD permit for the package boilers, and is now requesting a revision to the maximum steam production and heat input rates. Since SCC is requesting a change in the method of operation of the facility, the net increase in emissions must be determined by comparing the current actual emissions (i.e., PSD baseline emissions) to the proposed maximum emissions. PSD review is then required for the proposed modification for each pollutant for which the net increase in emissions exceeds specified PSD significant emission rates (i.e., a major modification).

Future maximum annual emissions for the new package boilers were presented previously in Table 2-4. The PSD baseline emissions for the package boilers are presented in Table 3-2. The PSD source applicability analysis, based on the current actual and the future annual emissions, is presented in Table 3-3. As shown in Table 3-3, the increase in emissions for all pollutants except NOx will not exceed the PSD significant emission rates. Therefore, the proposed modification is subject to PSD review for NOx.

Table 3-1. PSD Significant Emission Rates and De Minimis Monitoring Concentrations

,	Regulated	Significant Emission Rate	De Minimis Monitoring Concentration
Pollutant	Under	(TPY)	(μg/m³)
Sulfur Dioxide	NAAQS, NSPS	40	13, 24-hour
Particulate Matter (TSP)	NSPS	25	NA
Particulate Matter (PM10)	NAAQS	15	10, 24-hour
Nitrogen Oxides	NAAQS, NSPS	40	14, annual
Carbon Monoxide	NAAQS, NSPS	100	575, 8-hour
Volatile Organic Compounds (Ozone)	NAAQS, NSPS	40	100 TPY <sup>a</sup>
Lead	NAAQS	0.6	0.1, 3-month
Sulfuric Acid Mist	NSPS	7	NM ·
Total Fluorides	NSPS	3	0.25, 24-hour
Mercury	NESHAP	0.1	0.25, 24-hour
Total Reduced Sulfur	NSPS	10	10, 1-hour
Reduced Sulfur Compounds	NSPS	10	10, 1-hour
Hydrogen Sulfide	NSPS	10	0.2, 1-hour
MWC Organics (as dioxin/furan)	NSPS	$3.5 \times 10^{-6}$	NA
MWC Metals (as PM)	NSPS	15	NA
MWC Acid Gases (as SO <sub>2</sub> +HCl)	NSPS	40	NA
MSW Landfill Emissions (as NMVOC)	NSPS	50	NA

Note: Ambient monitoring requirements for any pollutant may be exempted if the impact of the increase in emissions is below *de minimis* monitoring concentrations.

MWC = Municipal waste combustor

MSW = Municipal solid waste

NA = Not Applicable

NAAQS = National Ambient Air Quality Standards

NESHAP = National Emission Standards for Hazardous Air Pollutants

NM = No ambient measurement method

NMVOC = Non-methane volatile organic compounds

NSPS = New Source Performance Standards

PM10 = particulate matter with aerodynamic diameter less than or equal to 10 micrometers

PSD = prevention of significant deterioration

TPY = tons per year

TSP = total suspended particulate matter

 $\mu g/m^3 = micrograms per cubic meter$ 

Source: F.A.C., Rule 62-212.400, Tables 212.400-2 and 212.400-3.

No de minimis concentration; an increase in VOC emissions of 100 TPY or more will require monitoring analysis for ozone.

Table 3-2. Estimated Baseline Annual Emissions for Existing Package Boilers (total all boilers), Stone Container Corporation

	I	No. 2 Fuel Oil			Natural Gas		Total
Regulated Pollutant	Emission Factor (a)	Annual Activity Factor (b)	Annual Emissions (TPY)	Emission Factor (a)	Annual Activity Factor (b)	Annual Emissions (TPY)	Annual Emissions (TPY)
Criteria and Precursor Polluta	nts						
Particulate Matter (PM)	0.0145 lb/MMBtu	0 MMBtu/yr	0.0	0.0050 lb/MMBtu	251,000 MMBtu/yr	0.63	0.6
Particulate Matter (PM10)	0.0072 lb/MMBtu	0 MMBtu/yr	0.0	0.0050 lb/MMBtu	251,000 MMBtu/vr	0.63	0.6
Sulfur dioxide	0.052 lb/MMBtu	0 MMBtu/vr	0.0	0.0006 lb/MMBtu	251,000 MMBtu/yr	0.08	0.0
Nitrogen oxides	0.05 lb/MMBtu	0 MMBtu/yr	0.0	0.05 lb/MMBtu	251,000 MMBtu/yr	6.28	6.2
Carbon monoxide	0.0216 lb/MMBtu	0 MMBtu/yr	0.0	0.0209 lb/MMBtu	251,000 MMBtu/yr	2.62	2.6
voc	0.0014 lb/MMBtu	0 MMBtu/yr	0.0	0.0014 lb/MMBtu	251,000 MMBtu/yr	0.18	0.1
Lead - Total	8.90E-06 lb/MMBtu	0 MMBtu/yr	0.0	2.71E-07 lb/MMBtu	251,000 MMBtu/yr	3.40E-05	3.40E-0
Designated Pollutants							
Sulfuric Acid Mist	8.88E-04 lbs/MMBtu	0 MMBtu/yr	0.0	_			0.
Fluorides - Total	3.20E-05 lbs/MMBtu	0 MMBtu/yr	0.0		-		0.
Hazardous Air Pollutants							
Beryllium	2.50E-06 lbs/MMBtu	0 MMBtu/yr	0.0	_			0.
Mercury	3.00E-06 lbs/MMBtu	0 MMBtu/yr	0.0	1.50E-10 lbs/MMBtu	251.000 MMBtu/vr	1.88E-08	1.88E-0

<sup>(</sup>a) Obtained from Table 2-3, except for NOx, which is based on CEM data for 1997.(b) Based on actual average fuel usage for 1996-1997. Fuel heating value assumed at 138,000 Btu/gal for oil and 1,000 BTU/scf for gas.

Table 3-3. PSD Source Applicability Analysis, SCC Package Boiler Modification

	Current	Maximum		Significant	PSD
	Actual	Future	Net	Emission	Review
Regulated	Emissions	<b>Emissions</b>	Change	Rate	Applies
Pollutant	(TPY)	(TPY)	(TPY)	(TPY)	?
<u>'.</u>					
Particulate (TSP)	0.63	20.9	20.3	25	No
Particulate (PM 10)	0.63	15.5	14.9	15	No
Sulfur dioxide	0.08	39.8	39.7	40	No
Nitrogen oxides	6.28	310	303.7	40	Yes
Carbon monoxide	2.62	58.4	55.8	100	No
Volatile organic compds.	0.18	3.88	3.70	40	No
Lead	3.40E-05	0.0072	0.0072	0.6	No
Mercury	1.88E-08	0.0022	0.0022	0,1	No
Fluorides	0.0	0.024	0.024	3	No
Sulfuric acid mist	0.0	0.66	0.66	7	No

## 4.0 AMBIENT MONITORING ANALYSIS

# **4.1 MONITORING REQUIREMENTS**

The CAA Amendments of 1977 require that the owner or operator of any proposed major new source or major modification conduct ambient air monitoring for applicable pollutants. As discussed in the source applicability section, Section 3.0, only NO<sub>x</sub> requires an air quality analysis to meet PSD preconstruction monitoring requirements for the proposed SCC modification. Monitoring must be conducted for a period of up to 1 year prior to submission of a construction permit application. However, if the increase in impacts due to the proposed new source or modification is less than the PSD *de minimis* monitoring concentrations, the applicant may be exempted from the PSD preconstruction monitoring requirements. For NO<sub>x</sub>, the *de minimis* level is  $14 \mu g/m^3$ , annual average (measured by NO<sub>2</sub>). As demonstrated in Section 6.0, the predicted maximum increase in annual average NO<sub>x</sub> impacts due to the proposed modification at SCC is  $1.2 \mu g/m^3$ . As a result, the proposed modification may be exempted from preconstruction NO<sub>x</sub> monitoring.

# **4.2 BACKGROUND NO, CONCENTRATIONS**

A background NO<sub>2</sub> concentration must be estimated to account for NO<sub>x</sub> sources which are not explicitly included in the atmospheric dispersion modeling analysis. In order to estimate a conservative background NO<sub>2</sub> concentration, a review of recent, available NO<sub>2</sub> monitoring data in the area of SCC was performed.

Presented in Table 4-1 is a summary of ambient NO<sub>2</sub> data available for 1996 and for January through September 1997, for all monitors located within Duval county. A total of one station is located in Duval county which has a continuous NO<sub>2</sub> monitor. The monitor is operated by the City of Jacksonville. Data recoveries exceed 93 percent for the station.

Annual average, and 1-hour maximums for  $NO_2$  are shown in Table 4-1. Since the monitor is located in an area of multi source emissions (point and mobile sources), these concentrations are expected to include substantial contributions from sources in the area. These potential major contributing sources are explicitly included in the modeling analysis (refer to Section 6.0). As a result, these concentrations are not representative of actual background concentrations that would be expected to occur in conjunction with the worst-case meteorology. However, in order to be

conservative, a 28  $\mu$ g/m³ annual average concentration, recorded at a site in Kooker Park was used as the background concentration in the modeling analysis.

Table 4-1. Summary of Ambient NO<sub>2</sub> Data for Sites in Duval County 1996 - 1997

SAROAD Site No.		Monitoring		No. of	Percent Data	N	IO <sub>2</sub> Concentration (μg/m³)
	City/Site	Method	Period	Obs.	Recovery	1-Hour	Annual Average
1960-032-H02	Jacksonville	Continuous	1996	8,148	93.0	150	28
	Kooker Park		1997(Jan-Sep)	6,288	95.7	130	25

Note:

No. = number.

Obs. = observations.  $NO_2$  = nitrogen dioxide.

 $\mu$ g/m<sup>3</sup> = micrograms per cubic meter.

Source: Florida DEP, 1996, 1997.

## 5.0 CONTROL TECHNOLOGY REVIEW

#### **5.1 GENERAL**

The control technology review requirements of the federal and state PSD regulations require that all applicable federal and state emission-limiting standards be met, and that BACT be applied to control emissions from the proposed or modified source. The BACT requirements are applicable to all regulated pollutants for which the increase in emissions from the new facility or modification exceeds the significant emission rate.

# BACT is defined in 40 CFR 52.21 as:

An emissions limitation, including a visible emission standard, based on the maximum degree of reduction of each pollutant emitted which the department, on a case by case basis, taking into account energy, environmental, and economic impacts, and other costs, determines is achievable through application of production processes and available methods, systems, and techniques (including fuel cleaning or treatment or innovative fuel combustion techniques) for control of such pollutant. If the Department determines that technological or economic limitations on the application of measurement methodology to a particular part of a source or facility would make the imposition of an emission standard infeasible, a design, equipment, work practice, operational standard or combination thereof, may be prescribed instead to satisfy the requirement for the application of BACT. Such standard shall, to the degree possible, set forth the emissions reductions achievable by implementation of such design, equipment, work practice, or operation.

The requirements for BACT were promulgated within the framework of PSD in the 1977 amendments of the CAA [Public Law 95-95; Part C, Section 165(a)(4)]. The primary purpose of BACT is to optimize consumption of PSD air quality increments and thereby enlarge the potential for future economic growth without significantly degrading air quality (EPA, 1978; 1980). Guidelines for the evaluation of BACT can be found in EPA's Guidelines for Determining Best Available Control Technology (BACT) (EPA, 1978) and in the PSD Workshop Manual (EPA, 1980). These guidelines were promulgated by EPA to provide a consistent approach to BACT and to ensure that the impacts of alternative emission control systems are measured by the same set of parameters. In addition, through implementation of these guidelines, BACT in one area may not be identical to BACT in another area. According to EPA (1980):

BACT analyses for the same types of emissions unit and the same pollutants in different locations or situations may determine that different control strategies should be applied to the different sites, depending on site-specific factors. Therefore, BACT analyses must be conducted on a case-by-case basis.

The BACT requirements are intended to ensure that the control systems incorporated in the design of a proposed facility reflect the latest in control technologies used in a particular industry and take into consideration existing and future air quality in the vicinity of the proposed facility. BACT must, as a minimum, demonstrate compliance with NSPS for a source (if applicable). An evaluation of the air pollution control techniques and systems, including a cost-benefit analysis of alternative control technologies capable of achieving a higher degree of emission reduction than the proposed control technology, is required. The cost-benefit analysis requires the documentation of the materials, energy, and economic penalties associated with the proposed and alternative control systems, as well as the environmental benefits derived from these systems. A decision on BACT is to be based on sound judgment, balancing environmental benefits with energy, economic, and other impacts (EPA, 1978).

Historically, a bottom-up approach consistent with the BACT Guidelines and PSD Workshop Manual has been used. With this approach, an initial control level, which is usually NSPS, is evaluated against successively more stringent controls until a BACT level is selected. However, EPA developed a concern that the bottom-up approach was not providing the level of BACT decisions originally intended. As a result, in December 1987, the EPA Assistant Administrator for Air and Radiation mandated changes in the implementation of the PSD program including the adoption of a new "top-down" approach to BACT decision-making.

The top-down BACT approach essentially starts with the most stringent (or top) technology and emissions limits that have been applied elsewhere to the same or a similar source category. The applicant must next provide a basis for rejecting this technology in favor of the next most stringent technology or propose to use it. Rejection of control alternatives may be based on technical or economic infeasibility. Such decisions are made on the basis of physical differences (e.g., fuel type), locational differences (e.g., availability of water), or significant differences that may exist in the environmental, economic, or energy impacts. The differences between the proposed facility and the facility on which the control technique was applied previously must be justified. The EPA issued a draft guidance document on the top-down approach entitled Top-Down Best Available Control Technology Guidance Document (EPA, 1990). However, to date EPA has not promulgated the top-down approach for determining BACT.

# **5.2 APPLICABILITY**

For the proposed SCC modification, NO<sub>x</sub> emissions are subject to PSD review. As a result, NO<sub>x</sub> emissions are subject to BACT review. According to the federal PSD regulations, a major modification must apply BACT for these pollutants for each emissions unit which is being physically modified, or for which there is a change in the method of operation due to the proposed modification [40 CFR 52.21(j)]. A change in the method of operation does not include an increase in the production rate or in the hours of operation, unless such increase would be prohibited by a federally enforceable permit condition established after January 6, 1975.

Package Boiler Nos. 1-3 will not be physically modified as part of the proposed increase in heat input and steam production. The existing package boilers are currently capable of the higher heat input and production rate. However there will be a change in the method of operation of the boilers. Therefore a BACT determination is required for Boiler Nos. 1-3 for NO<sub>x</sub> emissions.

Boiler Nos. 1-3 are also subject to BACT for particulate matter (PM) and sulfur dioxide (SO<sub>2</sub>). According to Rule 62-296.406 F.A.C, new and existing fossil fuel steam generators with less than 250 MMBtu/hr heat input are required to apply BACT for PM and SO<sub>2</sub>.

## 5.3 BACT FOR NO<sub>x</sub> EMISSIONS

Each of the existing Boiler Nos. 1-3 at SCC currently are permitted to operate at 174.5 MMBtu/hr and 125,000 lb of steam produced/hr, fired by natural gas and No. 6 fuel oil as backup. SCC is proposing to increase each of the boiler's maximum hourly heat input and steam production to 215 MMBtu/hr and 150,000 lb/hr, respectively, while maintaining the currently permitted emission limits.

#### 5.3.1 Existing Control Technology

Package Boiler Nos. 1-3 are currently equipped with low-NO<sub>x</sub> burners and utilize flue gas recirculation (FGR) to control NO<sub>x</sub> emissions. Each the three boiler's currently permitted emission limits are 0.2 lb/MMBtu, 34.94 lb/hr and 153.1 TPY for NO<sub>x</sub>. The current technology is adequate to meet the allowable emission limits.

SCC obtained permission from FDEP to conduct continuous NO<sub>x</sub> emission monitor relative accuracy testing (RATA) while operating near the proposed increased steam rate of 150,000 lb/hr to determine

emission estimates for this proposed project. The RATA test data is summarized in Table 5-1.  $NO_x$  emission rates ranged from 0.0918 to 0.1318 lb/MMBtu for steam rates ranging from approximately 141,000 lb/hr to 146,000 lb/hr.

## 5.3.2 Control Technology Review

A review of the RACT/BACT/LAER Clearinghouse (RBLC) was conducted to identify BACT determinations which have been issued for natural gas-fired boilers. A complete listing of these determinations is provided in Appendix C. This listing is presented chronologically, starting with the most recent determinations. Based on this listing, all determinations for boilers within the size range of 100 to 300 MMBtu/hr were identified. These determinations, which represent the size category of SCC's boilers, are presented in Table 5-2. These determinations are presented in the order of least stringent to most stringent emission rate. As shown, all BACT determinations, within the 100 to 300 MMBtu/hr range, were based on low-NO<sub>x</sub> burners, flue gas recirculation, or a combination of both. Previous BACT determinations have ranged from 0.05 lb/MMBtu to 0.20 lb/MMBtu. These determinations are generally for new boilers, and not existing boilers which were undergoing a steam rate increase.

Selective catalytic reduction (SCR) and selective non-catalytic reduction (SNCR) control systems can be identified as having practical potential for this application. Both of these systems are based on the reduction of NOx to N<sub>2</sub>, through a series of chemical reactions. SNCR has been determined as BACT for one boiler approximately four times as large as SCC's boilers, while no determinations were found requiring SCR as BACT for a natural gas-fired boiler. SCR and SNCR control systems are also costly to install. Therefore, SCR and SNCR were no longer considered feasible as BACT for Package Boiler Nos. 1-3.

#### 5.3.3 Proposed BACT

SCC's proposed NO<sub>x</sub> emission rate for Package Boiler Nos. 1-3 is 0.2 lb/MMBtu, 34.94 lb/hr and 153.1 TPY. Based on the RBLC, the proposed BACT for Package Boiler Nos. 1-3 is low-NO<sub>x</sub> burners and FGR.

# 5.4 BACT FOR PM/PM10 EMISSIONS

Based on the insignificant level of PM/PM10 emissions from Package Boiler Nos. 1-3, natural gas as the primary fuel was determined as BACT by PSD-FL-198 and is proposed as BACT for the proposed modification.

# 5.5 BACT FOR SO<sub>2</sub> EMISSIONS

Based on the insignificant level of SO<sub>2</sub> emissions from Package Boiler Nos. 1-3, natural gas as the primary fuel, and very low sulfur fuel oil with a maximum sulfur content of 0.05% as a backup fuel, was determined as BACT by PSD-FL-198 and is proposed as BACT for the proposed modification.

Table 5-1. Summary of 1998 RATA Test Data, Stone Container Corporation

Run No.	Steam Rate (lb/hr)	Emission Rate (lb/MMBtu)	
Boiler No. 1			
1	143,261	0.0918	
2	142,714	0.0923	
2 3 4	144,105	0.0924	
4	145,745	0.0918	
5	145,468	0.0925	
6	145,359	0.0925	
7	_ 145,464	0.0929	
8	145,791	0.0925	
9	144,891	0.0921	
10	144,941	0.0927	
Boiler No. 2			
. 1	142,480	0.1240	
2	143,141	0.1283	
2 3 4	143,900	0.1260	
	144,509	0.1277	
5	144,459	0.1284	
6	144,277	0.1277	
7	143,955	0.1317	
8	143,932	0.1318	
9	144,264	0.1311	
10	144,173	0.1301	
Boiler No. 3			
· . 1	141,764	0.1030	
2	142,318	0.1025	
3	142,745	0.1018	
4	142,768	0.1028	
5	142,932	0.1027	
6	143,018	0.1036	
7	143,609	0.1036	
8	143,495	0.1036	
9	143,559	0.1036	
10	143,836	0.1030	

Source: Source Testing and Consulting, Inc. (May 1998) and Stone Container Corporation

Table 5-2. Summary of BACT Determinations for NOx from 100 MMBtu/hr - 300 MMBtu/hr Boilers Fired by Natural Gas

Company	State	Permit No.	Permit Issue Date	Throughput	Emssion Limit	Control Equipment	Control Efficiency
LOCKPORT COGEN FACILITY	NY	292600 0446/00001-00007	07/14/93	210 MMBtu/hr	0.2 lb/MMBtu		
LAKEWOOD COGENERATION, L.P.	NJ		04/01/91	131 MMBtu/hr	0.2 lb/MMBtu	LOW NOX BURNERS	50
SARANAC ENERGY COMPANY	NY	5-942-106/1-9	07/31/92	249 MMBtu/hr	0.136 lb/MMBtu	LOW NOX BURNERS	
MINNESOTA CORN PROCESSORS, INC.	MN	AMENDMENT 6 TO 1939-88-0T-1	06/25/91	178.7 MMBtu/hr	0.125 lb/MMBtu	LOW NOX BURNERS	
GENERAL ELECTRIC CO.	IN	PSD (65) 1757	09/17/89	250 MMBtu/hr	0.12 lb/MMBtu	LOW NOX BURNERS, STAGED COMBUSTION AIR	
BERMUDA HUNDRED ENERGY LIMITED PARTNERSHIP	VA	51020	03/03/92	250 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNER	
SCOTT PAPER COMPANY	AL	503-2012	09/17/91	220.5 MMBtu/hr	0.1 lb/MMBtu	FACILITY NOW SHUT DOWN.	
NEWARK BAY COGENERATION PARTNERSHIP, L.P.	NJ	01-92-5231 TO 01-92-5261	06/09/93	206 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNERS, FLUE GAS RECIRCULATION (FGR)	
PILGRIM ENERGY CENTER	NY	472800 2054	·	204 MMBtu/hr	0.1 lb/MMBtu		
LAKEWOOD COGENERATION, L.P.	NJ		04/01/91	131 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNERS	50
NORTHERN CONSOLIDATED POWER	PA	25-328-1	05/03/91	100.4 MMBtu/hr	0.1 lb/MMBtu	<u>.</u>	
TRANSAMERICAN REFINING CORPORATION	LA	PSD-LA-571 (M-1)	02/10/95	244 MMBtu/hr	0.081 lb/MMBtu	LOW NOX BURNERS/COMBUSTION CONTROL	
AMERICAN CRYSTAL SUGAR COMPANY	MN	29B-92-OT-1	12/15/92	200.1 MMBtu/hr	0.075 lb/MMBtu	LOW NOX BURNER WITH FLUE GAS RECIRCULATION	
COURTAULDS FIBERS, INC.	AL	503-5002-X023 AND -X40	11/02/94	148 MMBtu/hr	0.070 lb/MMBtu	LOW NOX BURNERS WITH 8% FLUE GAS RECIRCULATION	87
JAMES RIVER CORP	MI	423-91	09/17/91	226.7 MMBtu/hr	0.06 lb/MMBtu	LOW NOX BURNERS AND FGR SYS	70
GRAIN PROCESSING CORP.	IN	CP 027-7239-00046	06/10/97	244 MMBtu/hr	0.05 lb/MMBtu	LOW NOX BURNERS AND FLUE GAS RECIRCULATION (FGR)	
NEWARK BAY COGENERATION PARTNERSHIP, L.P.	NJ	01-92-5231 TO 01-92-5261	06/09/93	200 MMBtu/hr	0.05 lb/MMBtu	LOW NOX BURNERS, FLUE GAS RECIRCULATION (FGR)	
ANITEC COGEN PLANT	NY	030200 0451	07/07/93	123 MMBtu/hr	0.05 lb/MMBtu	-	

Source: EPA's RACT/BACT/LAER Clearinghouse, 1998

## 6.0 AIR QUALITY IMPACT ANALYSIS

#### **6.1 SIGNIFICANT IMPACT ANALYSIS**

The general modeling approach followed EPA and FDEP modeling guidelines for determining compliance with AAQS and PSD increments. For all criteria pollutants that will be emitted in excess of the PSD significant emission rate due to a proposed project, a significant impact analysis is performed to determine whether the emission and/or stack configuration changes due to the project alone will result in predicted impacts that are in excess of the EPA significant impact levels at any location beyond the plant property boundaries.

Generally, if the facility undergoing the modification also is within 200 kilometers of a PSD Class I area, then a significant impact analysis is also performed for the PSD Class I area. Currently, the National Park Service (NPS) has recommended significant impact levels for PSD Class I areas. The recommended levels have not been promulgated as rules.

If the project's impacts are above the significant impact levels, then a more detailed air modeling analysis that includes background sources is performed. Current FDEP policies stipulate that the highest annual average and highest short-term (i.e., 24 hours or less) concentrations are to be compared to the applicable significant impact levels. Based on the screening modeling analysis results, additional modeling refinements with a denser receptor grid are performed, as necessary, to obtain the maximum concentration. Modeling refinements are performed with a receptor grid spacing of 100 meters (m) or less.

# **6.2 AAQS/PSD MODELING ANALYSIS**

For each pollutant for which a significant impact is predicted, a refined impact analysis is required. This analysis must consider other nearby sources and background concentrations and predict concentrations for comparison to ambient standards. In general, when 5 years of meteorological data are used in the analysis, the highest annual and the highest, second-highest (HSH) short-term concentrations are compared to the applicable AAQS and allowable PSD increments. The HSH concentration is calculated for a receptor field by:

- 1. Eliminating the highest concentration predicted at each receptor,
- 2. Identifying the second-highest concentration at each receptor, and
- 3. Selecting the highest concentration among these second-highest concentrations.

This approach is consistent with air quality standards and allowable PSD increments, which permit a short-term average concentration to be exceeded once per year at each receptor.

To develop the maximum short-term concentrations for the proposed project, the modeling approach was divided into screening and refined phases to reduce the computation time required to perform the modeling analysis. For this study, the only difference between the two modeling phases is the density of the receptor grid spacing employed when predicting concentrations. Concentrations are predicted for the screening phase using a coarse receptor grid and a 5-year meteorological data record.

(7)

If the original screening analysis indicates that the highest concentrations are occurring in a selected area(s) of the grid and, if the area's total coverage is too vast to directly apply a refined receptor grid, then an additional screening grid(s) will be used over that area. The additional screening grid(s) will employ a greater receptor density than the original screening grid, so refinements can be performed if necessary.

Refinements of the maximum predicted concentrations are typically performed for the receptors of the screening receptor grid at which the highest and/or HSH concentrations occurred over the 5-year period. Generally, if the maximum concentration from other years in the screening analysis are within 10 percent of the overall maximum concentration, then those other concentrations are refined as well. Typically, if the highest and HSH concentrations are in different locations, concentrations in both areas are refined.

Modeling refinements are performed for short-term averaging times by using a denser receptor grid, centered on the screening receptor to be refined. The angular spacing between radials is 2 degrees and the radial distance interval between receptors is 100 m. Annual modeling refinements employ an angular spacing between radials of 2 degrees and a distance interval from 100 to 300 m, depending on the concentration gradient in the vicinity of the screening receptor to be refined. If the maximum screening concentration is located on the plant property boundary, additional plant boundary receptors are input, spaced at a 2 degree angular interval and centered on the screening receptor. The domain of the refinement grid will extend to all adjacent screening receptors. The air dispersion model is then executed with the refined grid for the entire year of meteorology during which the screening concentration occurred. This approach is used to ensure that a valid HSH concentration is obtained. A more detailed description of the model, along with the emission inventory, meteorological data, and screening receptor grids, is presented in the following sections.

## 6.2.1 Model Selection

The Industrial Source Complex Short-term (ISCST3, Version 97363) dispersion model (EPA, 1995) was used to evaluate the pollutant impacts due to the proposed modification to Stone Container Corporation's (SCC) Jacksonville plant package boilers. This model is maintained on the EPA's Technical Transfer Network (TTN) internet web site. A listing of ISCST3 model features in presented in Table 6-1. The ISCST3 model is applicable to sources located in either flat or rolling terrain where terrain heights do not exceed stack heights. The ISCST3 model is designed to calculate hourly concentrations based on hourly meteorological parameters (i.e., wind direction, wind speed, atmospheric stability, ambient temperature, and mixing heights).

In this analysis, the EPA regulatory default options were used to predict all maximum impacts. Based on the land-use within a 3-km radius of the SCC site, the rural dispersion coefficients were used in the modeling analysis. The ISCST3 model was used to provide maximum concentrations for the annual and 24-hour averaging times.

#### 6.2.2 Meteorological Data

Meteorological data used in the ISCST3 model to determine air quality impacts consisted of a concurrent 5-year period of hourly surface weather observations and twice-daily upper air soundings from the National Weather Service (NWS) stations at Jacksonville International Airport (JAX) and Waycross, GA, respectively. The 5-year period of meteorological data was from 1983 through 1987. The NWS station at Jacksonville International Airport, located approximately 12 km to the southwest of the SCC plant site, was selected for use in the study because it is the closest primary weather station to the study area that is representative of the plant site.

#### **6.2.3 Emission Inventory**

#### Significant Impact Analysis

The future NOx emission rate and the physical and operational stack parameters for the package boilers' stack are summarized in Table 6-2. This table is based on emission and stack parameter data presented in Section 2.0. Because the current actual emission rate for the package boilers is very small (<10 TPY), the significant impact analysis was based on the future package boiler's emission rate of 310 TPY. All SCC sources were modeled at locations that are relative to the SCC plant baseline, which is the same modeling origin that was used in a previous PSD application for Seminole Kraft Corporation (KBN, 11/92).

# **AAQS Analysis**

An emission inventory of updated competing  $NO_X$  facilities were obtained from the FDEP. Supplemental emission data from FDEP's 1993 APIS data were used to provide emission estimates for several sources whose potential or allowable  $NO_X$  emissions were not available in the latest FDEP data.

From these data, a list of competing NO<sub>x</sub> facilities and their locations relative to the SCC plant location was developed and is provided in Table 6-3. An alphabetical listing of the inventory presented in Table 6-3 is included in Table D-1, Appendix D. All facilities were evaluated with the North Carolina screening technique to determine if they should be included in the AAQS or PSD Class II modeling analysis. Based on this technique, facilities whose maximum annual emissions in tons/year do not exceed the threshold quantity of 20 x (D-D1), where D1 is the proposed project's significant impact distance, were eliminated from air the modeling analysis.

A summary of the NO<sub>X</sub> source data that was used for the AAQS analysis is presented in Attachment E, Tables E-1 and E-2. Table E-1 presents the source information for all modeled facility emission points. In Table E-2, some sources are combined based on EPA's method for merging sources (EPA, 1992). In general, prominent emission sources within a facility were kept separate (i.e., no merging was performed). Numerous small emission sources within a facility were usually

$$M = \underline{h_s V T_s}$$

$$Q$$

merged into one source based on the following approach: for each stack, the mearged-stack parameter M was computed as follows:

where: M = merged stack parameter which accounts for the relative influence of stack height, plume rise, and emission rate on concentrations

 $h_s = \text{stack height (m)}$ 

 $V = (/4) dv_s = stack gas volumetric flow rate (m<sup>3</sup>/s)$ 

 $d_s = inside stack diameter (m)$ 

 $v_s = stack gas exit velocity (m/s)$ 

 $T_s$  = stack gas exit temperature (K)

Q = pollutant emission rate (g/s)

The parameters for the stack with the lowest value of M were used for the representative stack in the air modeling analysis. Then, the sum of the emissions from all applicable sources was assumed to be emitted from the representative stack.

#### **PSD Class II Analysis**

Of the facilities considered in the air modeling analysis, only the SCC and Cedar Bay Cogeneration facilities affect the NO<sub>2</sub> PSD increment. The package boilers and the Cedar Bay facility are PSD increment consuming sources. There are also several SCC sources that have been shut down since the 1988 baseline date that would expand PSD increment in the vicinity of the plant. The Jacksonville Electric Authority's St. John's River Power Power is not a PSD source for NO<sub>x</sub>, as the plant was under construction prior to the 1988 baseline date.

A summary of SCCs NO<sub>x</sub> emissions and source stack parameters for the PSD baseline year (1988-89) are provided in Tables 6-4 and 6-5, respectively. These sources, together with the package boilers and the Cedar Bay sources, comprise the PSD Class II emission inventory for the proposed project.

#### **PSD Class I Analysis**

Because the proposed package boiler expansion's maximum air impacts do not exceed the recommended NPS significant impact levels for NO<sub>x</sub> at the Okefenokee NWA PSD Class I area, a PSD Class I increment consumption modeling assessment was not required.

# **6.2.4 RECEPTOR LOCATIONS**

#### 6.2.4.1 Site Vicinity

To determine the NO<sub>x</sub> significant impact area for the proposed project, concentrations were predicted for 180 regular and 170 discrete polar grid receptors located in a radial grid centered on SCC's plant baseline location, the selected modeling origin. Receptors were located in "rings" with 36 receptors per ring, spaced at 10-degree intervals and at distances of the fenceline 1.5, 2, 3, 4, and 5 km from the origin. Discrete receptors included 36 receptors located on the plant property boundary at 10 degree intervals, plus 134 additional off-property receptors at distances of 0.4, 0.6, 0.8, 1.0 and 1.2 km from the origin to cover the area between the property boundary and the closest regular receptor grid distance (i.e., 1.5 km). The 36 property boundary receptors used for the screening analysis are presented in Table 6-6.

Based on the results of the significant impact analysis, the proposed project was determined to be marginally over the significant impact level and out to a distance of approximately 600 m from the origin. Based on this results, a maximum receptor distance of 1 km was used for the screening grid for the AAQS and PSD Class II analysis.

#### 6.2.4.2 Class I Area

Impacts for the proposed modification only were also compared to the Class I significance level recommended by the National Park Service (NPS). Maximum NO<sub>x</sub> impacts at the Okefenokee and Wolf Island NWA's were predicted using 11 discrete receptors located along the southern and/or eastern borders of the respective PSD Class I areas. A listing of Class I receptors used in the air modeling analysis is provided in Table 6-7.

#### 6.2.5 BACKGROUND CONCENTRATIONS

To estimate total air quality concentrations, a background concentration must be added to the modeling results. The background concentration is considered to be the air quality concentration contributed by sources not included in the modeling evaluation.

The derivation of the background concentration for the modeling analysis was presented in Section 4.0. The only ambient monitoring station currently measuring  $NO_2$  in Duval County is located at Kooker Park in Jacksonville. Based on the analysis of these data, a  $NO_X$  background concentration of  $28 \, \mu \text{g/m}^3$  was selected. The background concentration was added to the maximum model-predicted concentration to estimate the total  $NO_X$  air quality level for comparison to the AAQS.

#### 6.2.6 BUILDING DOWNWASH EFFECTS

All significant building structures within SCC's and Cedar Bay's existing plant area were determined by inspection of a site plot plan. A total of 6 building structures were evaluated. All building structures were processed in the EPA Building Input Profile (BPIP, Version 95086) program to determine direction-specific building heights and projected widths for each 10-degree azimuth direction for each source that was included in the modeling analysis. A listing of dimensions for each structure is presented in Table 6-8.

#### **6.3 MODEL RESULTS**

#### 6.3.1 SIGNIFICANT IMPACT ANALYSIS

#### **Site Vicinity**

A summary of the predicted maximum  $NO_X$  concentration for the proposed modification only for the screening analysis is presented in Table 6-9. The modeling results indicate that the maximum screening analysis concentration of 1.23  $\mu$ g/m³ is above the significance level of 1.0  $\mu$ g/m³. It was further determined that the significant impact area for the proposed modification extends out approximately 600 m from the SCC plant baseline location.

# Okefenokee and Wolf Island NWA

A summary of the predicted maximum  $NO_X$  concentration for the proposed modification only at the two PSD Class I areas is presented in Table 6-10. The results indicate that the maximum predicted impact of  $0.009 \ \mu g/m^3$ , annual average, is below the NPS recommended significant impact level of  $0.03 \ \mu g/m^3$ , annual average.

#### **6.4 AAQS ANALYSIS**

A summary of the maximum annual  $NO_x$  concentration predicted for all sources for the screening analysis is presented in Table 6-11. Based on the proximity of the screening analysis maximum impact, additional modeling refinements were not performed. The maximum total  $NO_x$  impact is compared to the AAQS in Table 6-12. The maximum predicted annual concentration is  $39 \mu g/m^3$ , which includes a non-modeled background concentration of  $28 \mu g/m^3$ . The total  $NO_x$  concentration is less than the AAQS of  $100 \mu g/m^3$ .

#### 6.5 PSD CLASS II ANALYSIS

A summary of the maximum NO<sub>2</sub> PSD increment consumption for the screening analysis is presented in Table 6-13. The screening analysis results indicate that the PSD increment is less than zero (i.e., increment expansion) in all areas in the vicinity of the SCC plant. Therefore, additional modeling refinements were not performed.

#### 6.6 PSD CLASS I ANALYSIS

The maximum annual NO<sub>2</sub> concentration at the Okefenokee and Wolf Island NWAs due to the proposed project are below the NPS' recommended PSD Class I significant impact level. Therefore, a full PSD Class I incremental analysis is not required.

Table 1.3-10. EMISSION FACTORS FOR METALS FROM NO. 6 FUEL OIL COMBUSTION<sup>a</sup>

	Average Emission Factor <sup>b</sup>	EMISSION FACTOR
Metal	(lb/10 <sup>3</sup> Gal)	RATING
Antimony	5.25E-03°	E
Arsenic	1.32E-03	С
Barium	2.57E-03	· D
Beryllium	2.78E-05	C
Cadmium	3.98E-04	С
Chloride	3.47E-01	D
Chromium	8.45E-04	C
Chromium VI	2.48E-04	Ċ
Cobalt	6.02E-03	$\mathbf{D}^{\cdot}$
Copper	1.76E-03	C
Fluoride	3.73E-02	D
Lead	1.51E-03	С
Manganese	3.00E-03	С
Mercury	1.13E-04	С
Molybdenum	7.87E-04	D
Nickel	8.45E-02	С
Phosphorous	9.46E-03	D
Selenium	6.83E-04	С
Vanadium	3.18E-02	D
Zinc	2.91E-02	D

<sup>&</sup>lt;sup>a</sup> Data are for residual oil fired boilers, Source Classification Codes (SCCs) 1-01-004-01/04.

<sup>b</sup> References 64-72. To convert from lb/10<sup>3</sup> gal to kg/10<sup>3</sup> L, multiply by 0.12.

<sup>c</sup> References 29-32,40-44.

Table 1.3-11. DEFAULT CO<sub>2</sub> EMISSION FACTORS FOR LIQUID FUELS<sup>a</sup>

# EMISSION FACTOR RATING: B

Fuel Type	%C <sup>b</sup>	Density <sup>c</sup> (lb/gal)	Emission Factor (lb/10 <sup>3</sup> gal)
No. 1 (kerosene)	86.25	6.88	21,500
No. 2	87.25	7.05	22,300
Low Sulfur No. 6	87.26	7.88	25,000
High Sulfur No. 6	85.14	7.88	24,400

<sup>&</sup>lt;sup>a</sup> Based on 99% conversion of fuel carbon content to CO<sub>2</sub>. To convert from lb/gal to gram/cm<sup>3</sup>, multiply by 0.12. To convert from lb/10<sup>3</sup> gal to kg/m<sup>3</sup>, multiply by 0.12.

<sup>b</sup> Based on an average of fuel carbon contents given in references 73-74.

<sup>c</sup> References 73, 75.

Table 6-1. Major Features of the ISCST3 Model

#### ISCST3 Model Features

- Polar or Cartesian coordinate systems for receptor locations
- Rural or one of three urban options which affect wind speed profile exponent, dispersion rates, and mixing height calculations
- Plume rise due to momentum and buoyancy as a function of downwind distance for stack emissions (Briggs, 1969, 1971, 1972, and 1975; Bowers, et al., 1979).
- Procedures suggested by Huber and Snyder (1976); Huber (1977); and Schulman and Scire (1980) for evaluating building wake effects
- Procedures suggested by Briggs (1974) for evaluating stack-tip downwash
- Separation of multiple emission sources
- Consideration of the effects of gravitational settling and dry deposition on ambient particulate concentrations
- Capability of simulating point, line, volume, area, and open pit sources
- Capability to calculate dry and wet deposition, including both gaseous and particulate precipitation scavenging for wet deposition
- Variation of wind speed with height (wind speed-profile exponent law)
- Concentration estimates for 1-hour to annual average times
- Terrain-adjustment procedures for elevated terrain including a terrain truncation algorithm for ISCST3; a built-in algorithm for predicting concentrations in complex terrain
- Consideration of time-dependent exponential decay of pollutants
- The method of Pasquill (1976) to account for buoyancy-induced dispersion
- A regulatory default option to set various model options and parameters to EPA recommended values (see text for regulatory options used)
- Procedure for calm-wind processing including setting wind speeds less than 1 m/s to 1 m/s.

Note: ISCST3 = Industrial Source Complex Short-Term.

Source: EPA, 1995.

Table 6-2. Summary of Stack Parameters and NOx Emissions for the Modified Package Boilers, Stone Container

	Stack Heig	ght	Stack Diame	ter	Flowrate	Stack Veloc	city	Stack Te	emp.	NOx Em	issions
Source	(ft)	(m)	(ft)	(m)	(acfm)	(f/s)	(m/s)	(deg F)	(deg K)	(TPY)	(g/s)
Package Boilers 1-3	200	61.0	8.0	2.44	204,900	67.94	20.71	330	438.7	310	8.92

# Legend

ft = feet

m = meters

acfm = actual cubic feet per minute

f/s = feet per second

m,/s = meters per second

deg F = degrees Fahrenheit

deg K = degrees Kelvin

TPY = tons per year

g/s = grams per second

Table 6-3. NO<sub>X</sub> Screening Analysis for the AAQS and PSD Class II Inventories for Stone Container Corporation

							Screening	Maximum	AAQS and/or
			Relative to Stone Container Facility			Emission	Allowable	PSD Class II	
•	UTM Coo	rdinates (km)	X	Υ	Distance	Direction	Threshold	Emissions	Modeling
Facility Name	E	N	(km)	(km)	(km)	(degrees)	(TPY)(a)	(TPY)	Analysis?
Amerada Hess Jacksonville	442.7	3365.0	0.7	-0.6	0.9	131	SIA	28.8	YES
Cedar Bay Cogeneration, Inc.	441.1	3365.1	-0.9	-0.5	1.1	240	1	3,788	YES
Anheuser Busch, Inc Jacksonville	440.6	3366.8	-1.4	1.2	1.9	310	17	1,038	YES
Atlantic Coast Asphalt - Heckscher	440.0	3364.1	-2.0	-1.5	2.5	233	30	NA .	NO
Stone Container Corp	439.2	3365.5	-2.8	-0.1	2.8	269	36	NA	NO
Quickrete-Jacksonville	439.8	3363.3	-2.2	-2.3	3.2	224	44	, <b>9</b>	NO
J.B. Coxwell Contracting, Inc.	446.0	3365.9	4.0	0.3	4.0	85	59	47	NO
Interstate Brands Corporation	437.2	3366.3	-4.8	0.7	4.9	278	77	NA	NO
Jacksonville Electric Authority - SJRPP	446.9	3366.3	4.9	0.7	4.9	82	79	32,289	YES
City of Jacksonville - Solid Waste Division	446.5	3367.7	4.5	2.1	5.0	65	80	23	NO
U S Gypsum Co	438.9	3361.2	-3.1	-4.4	5.4	215	88	353	YES
Celotex Corp	446.4	3362.4	4.4	-3.2	5.5	126	90	76	NO
Jacksonville Electric Authority - Northside	447.7	3364.9	5.7	-0.7	5.7	97	95	15,286	YES
Support Terminal Operg. Part.,L.P.	438.5	3360.5	-3.5	-5.1	6.2	214	104	9	NO
PCS Phosphate- Jacksonville	439.3	3359.8	-2.7	-5.8	6.4	205	108	27	NO .
Jefferson Smurfit Corp (U.S.) - Jacksonville	439.9	3359.3	-2.1	-6.3	6.6	198	113	1,200	YES
Jacksonville Electric Authority - Kennedy	440.0	3359.2	-2.0	-6.4	6.7	197	114	4,245	YES
Millennium Specialty Chemicals	436.8	3360.7	-5.2	-4.9	· 7.1	227	122	189	YES
Coastal Fuels Marketing, Inc.	439.7	3358.7	-2.3	-6.9	7.3	198	125	16	NO
Jefferson Smurfit Corporation	440.0	3358.1	-2.0	-7.5	7.8	195	135	7	NO
BF Goodrich Co. Engineered Polymer Product	450.0	3365.5	8.0	-0.1	8.0	91	140	16	NO
Jacksonville Buckman Sewage Tretmnt Plnt	439.4	3357.7	-2.6	-7.9	8.3	198	146	NA	NO
Castleton Beverage Co	438.4	3373.9	-3.6	8.3	9.0	337	160	3	NO
Industrial Water Services, Inc.	439.5	3356.8	-2.5	-8.8	9.1	196	163	2	NO
Mulliniks Construction Co., Inc Portable Cr	433.7	3361.4	-8.4	-4.2	9,3	243	167	NA	NO
Turner Electric Works	438.2	3357.0	-3.8	-8.6	9.4	204	168	1	NO
Owens-Corning - Jacksonville	439.3	3356.0	-2.7	-9.6	10.0	196	179	15	NO
University Medical Center	436.5	3357.2	-5.5	-8.4	10,0	213	181	39	NO
Cookson Matthey Eagle	433.0	3358.5	-9.0	-7.1	11,5	232	209	NA	NO
Kraft Foods	437.5	3354.7	-4.5	-10.9	11.8	202	215	16	NO
Jacksonville Electric Authority - Southside	437.7	3353.9	-4.4	-11.8	12.5	200	231	1,349	YES
Gate Riverplace Co.	436.8	3354.2	-5.2	-11.4	12,6	204	231	74	NO
Pan Coatings Of Florida, Inc.	434.8	3355.1	-7.2	-10.5	12.7	214	234	NA	NO
Hardage Giddens Funeral Homes Of Jackson		3354.5	-7.2	-11,1	13.2	213	245	1	NO
Anchor Glass Container Corporation	431.3	3357.5	-10.7	-8,1	13.4	233	248	789	YES
Chemrock Corp	429.7	3359.6	-12.3	-6.0	13.7	244	254	2	NO
Atlantic Dry Dock Corporation	455.8	3361.7	13.8	-3.9	14.3	106	267	7	NO

Table 6-3. NO<sub>X</sub> Screening Analysis for the AAQS and PSD Class II Inventories for Stone Container Corporation

		,	·Polativ	e to Sto	ne Containe	r Facility	Screening Emission	Maximum Allowable	AAQS and/or PSD Class II
	UTM Coordinates (km)		Relative to Stone Contain  X Y Distance			Direction	Threshold	Émissions	Modeling
Facility Name	E	N N	(km)	(km)	(km)	(degrees)	(TPY)(a)		Analysis?
St Vincents Medical Center	434.6	3353.0	-7.4	-12.6	14.6	211	273	48	NO
Con Agra Feed Company	431.4	3355.3	-10.6	-10.3	14.8	226	276	NA	NO
Electro-Mechanical South, Inc.	427.0	3364.5	-15.0	-1,1	15.0	266	280	NA	NO
Baptist Medical Center	435.4	3352.0	-6.6	-13.6	15.1	206	282	773	YES
Wincup	428.2	3357.8	-13.8	-7.8	15.9	241	297	NA	NO
Metalplate Galvanizing	426.5	3362.0	-15.5	-3.6	15.9	257	298	NA	NO
General Electric Co	458.1	3364.5	16.1	-1.2	16.1	94	302	1	NO
Metal Container Corporation	428.4	3356.4	-13.6	-9.2	16.4	236	308	7	NO
Bush Boake Allen, Inc.	427.6	3357.3	-14.4	-8.3	16.6	240	312	96	NO
City Of Jacksonville(Girvin Rd Landfill)	455.4	3355.6	13.4	-10.0	16.7	127	315	77	NO
D-Graphics Div. Jefferson Smurfit Corp.	440.1	3348.4	-1.9	-17.2	17.3	186	326	NA	NO
Reichhold Chemicals, Inc.	428.2	3355.0	-13.8	-10.7	17.4	232	329	14	NO
St Luke's Hospital Association	443.8	3346.9	1.8	-18.8	18.8	175	357	9	NO
J S Naval Station Mayport	460.4	3361.6	18.4	-4.0	18.8	102	357	56	NO
S & G Packaging L.L.C.	442.5	3386.1	0.5	20.5	20.5	1	390	2	NO
First Union Bank Of Florida	444.0	3342.8	2.0	-22.8	22.9	175	438	357	NO
3 Thermal Remediation Group - Nas Jax	434.2	3343.7	-7.8	-21.9	23.2	200	444	4	NO
Jnited States Navy - Nas Jacksonville	434.2	3342.8	-7.8	-22.8	24.1	199	462	276	NO
Mayo Clinic Jacksonville	458.0	3347.5	16.0	-18.1	24.2	139	463	39	NO
Refuse Services, Inc.	442.3	3341.2	0.3	-24.4	24.5	179	469	14	NO
Ring Power Corp - Sunbeam Road	442.0	3341.0	0.0	-24.6	24.6	180	472	79	NO
David Coxwell	420.0	3353.7	-22.0	-11.9	25.0	242	481	23	NO
Duval Asphalt Products - Phillips Highway	441.8	3340.0	-0.2	-25.6	25.6	181	492	18	NO
Atlantic Coast Asphalt -,Shad	445.3	3339.7	3.3	-25.9	26.2	173	503	19	NO
Champion International Corp	416.5	3353.2	-25.5	-12.4	28.4	244	547	16	NO
Rayonier Inc.	454.7	3392.2	12.7	26.6	29.5	26	570	1,582	YES
J.B. Coxwell Contracting, Inc.	448.1	3336.6	6.1	-29.0	29.7	168	573	47	NO
Anderson Columbia, Inc #7	448.1	3336.5	6.1	-29.1	29.7	168	575	7	NO
Jefferson Smurfit Corp-Fernandina Beach	456.2	3394.2	14.2	28.6	31.9	26	619	5,058	YES
J S Naval Air Station - Cecil Field	415.2	3344.5	-26.8	-21.1	34.1	232	662	71	NO
Dawson Land Development, Co., Inc.	463.2	3335.6	21.2	-30.0	36.8	145	715	NA	NO
Dustcoating, Inc.	413.1	3342.9	-28.9	-22.7	36.8	232	715	8	NO
Ameristeel, Jacksonville,Mill Div.	405.9	3350.2	-36.1	-15.4	39.2	247	765	307	NO
Florida Solite Company	427.4	3326.5	-14.6	-39.1	41.7	200	815	108	NO
Tamko Roofing Products, Inc.	435.2	3316.8	-6.8	-48.8	49.3	188	965	NA	NO
E.I. Dupont DE Nemours & CO- Highland	398.7	3325.0	-43.3	-40.6	59.4	227	1167	NA	NO

Table 6-3. NO<sub>X</sub> Screening Analysis for the AAQS and PSD Class II Inventories for Stone Container Corporation

							Screening	Maximum	AAQS and/or
			Relativ	e to Sto	ne Containe	r Facility	Emission	Allowable	PSD Class II
	UTM Coo	rdinates (km)	X	Y	Distance	Direction	Threshold	Emissions	Modeling
Facility Name	E	N	(km)	(km)	(km)	(degrees)	(TPY)(a)	(TPY)	Analysis?

NA = Emissions not provided

- (a) Screening emissions threshold is 20 x [Distance (km) to facility -1 km], based on North Carolina Screening Method.

  A significant impact distance of 1 km was assumed for including competing NOx facilities into the inventory.

  Total screening area is 51 km from the SCC facility. All facilities emitting <1 TPY have been omitted.
- (b) Indicates PSD sources at this facility
  Stone Container Corporation Jacksonville facility UTM coordinates (km):
  442.0 3365.6
- (c) Sources within 1 km of the SCC site are modeled without regard to the screening criteria.

Source: Golder Associates, 1998

Table 6-4. PSD Baseline (1989) NOx Emission Data for the Stone Container Corporation a, Jacksonville

		1989-1990 Hours of	Annual Baselin	e NO <sub>v</sub> Emissions
Unit Description	Basis	Operation	tons/yr	g/s
ark Boiler No. 1	74.1 lb/hr; 1991 stack test	8,169	302.7	8.71
ark Boiler No. 2	45.9 lb/hr; 1991 stack test	7,877	180.8	5.2
ower Boiler No. 1	8,129,846 gal/yr; 67 lb/1000 gal	8,255	272.3	7.83
ower Boiler No. 2	8,581,041 gal/yr; 67 lb/1000 gal	8,472	287.5	8.27
ower Boiler No. 3	8,723,551 gal/yr; 67 lb/1000 gal	8,489	292.2	8.41
ecovery Boiler No. 1	28.8 lb/hr; 1991 stack test	8,203	118.1	3.4
ecovery Boiler No. 2	31.8 lb/hr; 1991 stack test	8,023	127.6	3.67
ecovery Boiler No. 3	34.3 lb/hr; 1991 stack test	8,019	137.5	3.96
nelt Dissolving Tank No. 1	<del></del>		0 ' '	0
melt Dissolving Tank No. 2			0	0
melt Dissolving Tank No. 3			0	0
me Kiln No. 1	15.3 lb/hr; 1991 stack test	1,781	13.6	0.39
me Kiln No. 2	10.7 lb/hr; 1991 stack test	7,284	39	1.12
me Kiln No. 3	15.9 lb/hr; 1991 stack test	7,460	<u>59.3</u>	<u>1.71</u>
	·	TOTALS	1,830.60	52.67

# Note:

gal = gallon.

g/s = gram per second.

lb/hr = pound per hour.

PSD = prevention of significant deterioration.

tons/yr = tons per year.

Source: 1989/1990 Annual Operating Reports submitted to FDER and stack tests.

<sup>&</sup>lt;sup>a</sup> Formerly Seminole Kraft Corporation

Table 6-5. PSD Baseline (1989) Stack and Operating Data for the Stone Container Facility - Jacksonville

	S	tack Height	Stac	k Diameter	\	/elocity	Tem	perature	
Unit Description	(ft)	(m)	(ft)	(m)	(ft/s)	(m/s)	(deg F)	(K)	Basis
Bark Boiler No. 1	136	41.45	8.08	2.46	42.7	13.01	138	332	1991 stack test data
Bark Boiler No. 2	136	41.45	8.08	2.46	42.7	13.01	138	332	1991 stack test data
Power Boiler No. 1	106	32.31	6	1.83	46	14.02	360	455	1991 stack test data
Power Boiler No. 2	106	32.31	7	2.13	47.6	14.51	330	439	1991 stack test data
Power Boiler No. 3	106	32.31	7	2.13	47.6	14.51	330	439	1991 stack test data
Recovery Boiler No. 1	126	38.4	8.5	2.59	52.4	15.97	155	341	1991 stack test data
Recovery Boiler No. 2	126	38.4	9	2.74	51.2	15.61	162	345	1991 stack test data
Recovery Boiler No. 3	126	38.4	9	2.74	47.9	14.6	159	344	1991 stack test data
Smelt Dissolving Tank No. 1	120	36.58	3.5	1.07	13	3.96	160	344	AES Cedar Bay SCA
Smelt Dissolving Tank No. 2	124	37.8	4	1.22	14	4.27	160 .	344	AES Cedar Bay SCA
Smelt Dissolving Tank No. 3	124	37.8	4	1.22	14	4.27	160	344	AES Cedar Bay SCA
Lime Kiln No. 1	69	21.03	5.8	1.77	10.2	3.11	158	343	Various stack test data
Lime Kiln No. 2	75	22.86	4.67	1.42	21.4	6.52	145	336	Various stack test data
Lime Kiln No. 3	75	22.86	3.67	1.12	26.8	8.17	145	336	Various stack test data

Note:

ft = feet.

PSD = prevention of significant deterioration.

m = meter.

ft/s = feet per second.

deg F = degrees Fahrenheit.

K = Kelvin.

<sup>&</sup>lt;sup>a</sup> Formerly Seminole Kraft Corporation

Table 6-6. SCC Property Boundary Receptors Used in the Modeling Analysis

Direction (deg)	Distance (m)	Direction (deg)	Distance (m)	
10	657	190	289	
20	636	200	276	
30	491	210	269	
40	410	220	271	
50	361	230	280	
60	332	240	270	
70	316	250	403	
80	310	260	427	
90	314	270	469	
100	328	280	482	
110	355	290	483	
120	. 400	300	450	
130	696	310	500	
140	678	320	595	
150	440	330	764	
160	346	340	1,113	
170	315	350	1,285	
180	297	360	1,243	

Note: Distances are relative to the SCC plant baseline location.

deg = degree.

m = meter.

Table 6-7. Wolf Island and Okefenokee Wilderness Area Receptors Used in the Modeling Analysis

	dinates (km)	DCD Class I Asse
East	North	PSD Class I Area
470.5	3,459.0	Wolf Island
391.0	3,417.0	Okefenokee
390.0	3,410.0	Okefenokee
392.0	3,400.0	Okefenokee
390.0	3,395.0	Okefenokee
391.0	3,390.0	Okefenokee
390.0	3,384.0	Okefenokee
383.0	3,382.0	Okefenokee
378.0	3,382.0	Okefenokee
374.0	3,383.0	Okefenokee
370.0	3,383.0	Okefenokee

Table 6-8. Building Structures Considered in the SCC Modeling Analysis

Structure	Height		Len	Length		Width	
· · · · · · · · · · · · · · · · · · ·	(ft)	(m)	(ft)	(m)	(ft)	(m)	
Recovery Boilers	90	27.43	156.7	47.78	80	24.38	
Pulp Mill	72	21.95	212.5	64.77	225	68.60	
Power Boilers	60	18.29	115	35.05	201	61.34	
Bark Boilers	60	18.29	75	22.86	67.5	20.57	
Package Boilers	20	6.10	90	27.43	40	12.19	
Ceder Bay Boilers	161	49.07	248	75.70	110	33.50	

Source Golder Associates Inc., 1998

Table 6-9. Maximum Predicted NO<sub>x</sub> Concentrations for the Proposed Package Boilers Only

		Receptor	Period	
Averaging	Concentration <sup>a</sup>	Direction	Distance	Ending
Time	$(\mu g/m^3)$	(degrees)	(m)	(YYMMDDHH)
nual	1.14	120	400	83123124
	0.84	110	438	84123124
	1.23	120	400	85123124
	0.81	110	438	86123124
	1.07	120	400	87123124
IGH 24-Hour	18.1	120	400	83042424
	18.3	110	438	84022924
	22.8	110	438	85021224
	16.2	110	438	86030224
	16.4	120	400	87010224
HGH 8-Hour	43.	120	400	83041708
	27.	120	400	84032924
	34.	110	438	85011508
	42.	110	438	86030208
	36.	110	355	87031008
GH 3-Hour	81.	120	400	83041706
	53.	130	696	84110524
	63.	110	438	85051703
	70.	110	438	86030206
	55.	110	355	87031003
GH 1-Hour	115.	110	355	83071723
	114.	110	355	84091105
•	115.	110	355	85060202
	112.	120	400	86050224
	110.	110	355	87102902

Note: YY=Year, MM=Month, DD=Day, HH=Hour

Maximum concentrations indicated are for the proposed package boilers only with no offsets.
 All receptor coordinates are reported with respect to the SKC plant baseline location.

Table 6-10. Maximum Predicted NO<sub>X</sub> Impacts Due to the Proposed Package Only at the Okefenokee and Wolf Island NWAs

		Receptor 1		Period
Averaging	Concentration	Direction	Distance	Ending
Time	(μg/m³)	(degrees)	(m)	(YYMMDDHH)
Annual	0.008	391000	3417000	83123124
	0.009	392000	3400000	84123124
	0.008	391000	3390000	85123124
	0.009	390000	3395000	86123124
	0.009	391000	3417000	87123124
ligh 24-Hour	0.13	390000	3384000	83080124
	0.16	391000	3417000	84061424
	0.20	391000	3390000	85022324
	0.17	391000	3417000	86030924
	0.16	392000	3400000	87051124
IIGH 8-Hour	0.39	390000	3410000	83022208
	0.45	390000	3395000	84072124
	0.38	390000	3395000	85050124
	0.39	392000	3400000	86111124
	0.40	392000	3400000	87091424
HIGH 3-Hour	0.61	390000	3410000	83081721
	0.84	390000	3395000	84072121
	0.75	391000	3417000	85112624
	0.70	392000	3400000	86102421
	0.80	392000	3400000	87091421
HIGH 1-Hour	1.52	390000	3384000	83091223
	1.60	392000	3400000	84101719
	1.71	391000	3390000	85080720
	1.70	391000	3390000	86012119
	1.47	391000	3390000	87082121

Note: YY=Year, MM=Month, DD=Day, HH=Hour.

<sup>&</sup>lt;sup>a</sup> All receptor coordinates are reported with respect to the SCC plant baseline location.

Table 6-11 Maximum Predicted NO<sub>x</sub> Impacts in the Vicinity of the SCC Mill, Due to All Sources - Screening Analysis

Averaging Time		Receptor I	Period	
	Concentration (μg/m³)	Direction (degrees)	Distance (m)	Ending (YYMMDDHH)
Annual	10.86	250	185	83123124
	11.04	240	235	84123124
	10.90	250	185	85123124
	10.10	240	235	86123124
	10.94	320	800	87123124

Note: YY=Year, MM=Month, DD=Day, HH=Hour.

<sup>&</sup>lt;sup>a</sup> All receptor coordinates are reported with respect the SCC plant baseline location.

Table 6-12. Maximum Predicted NO<sub>2</sub> Concentrations Compared to the AAQS

Averaging Time	Total Concentration (µg/m³)	Modeled Concentration (μg/m³)	Background Concentration (μg/m³)	Receptor I Direction (degrees)	Distance (m)	AAQS (μg/m³)
Annual	39	11	28	240	235	100

Note: YY=Year, MM=Month, DD=Day, HH=Hour

<sup>&</sup>lt;sup>a</sup> Receptor coordinates are with respect to the SCC plant baseline location.

Table 6-13. Maximum Predicted NO<sub>2</sub> PSD Class II Increment Consumption in the Vicinity of the SCC Plant Site - Screening Analysis

		Receptor	Location <sup>b</sup>	Period
Averaging Time	Concentration (µg/m³)	Direction (degrees)	Distance (m)	Ending (YYMMDDHH)
ınnual	< 0.0		<u>-</u>	83123124
	< 0.0	<u>.</u>	-	84123124
	< 0.0	•	-	85123124
	< 0.0	· -	-	86123124
	< 0.0		-	87123124

Note: m = meter.

PDS = prevention of significant deterioration.

 $NO_2$  = nitrogen dioxide.

 $\mu$ g/m³ = micrograms per cubic meter. YYMMDDHH = year, month, day, hour.

<sup>&</sup>lt;sup>a</sup> Relative to the location of the SCC plant base line location.

#### 7.0 ADDITIONAL IMPACT ANALYSIS

# 7.1 INTRODUCTION

SCC is proposing to increase the steam rate of its existing boilers at the Jacksonville mill. The modification is subject to the PSD new source review requirements for NO<sub>x</sub>. The additional impact analysis and the Class I area analysis address this pollutant.

The analysis addresses the potential impacts on vegetation, soils, and wildlife of the surrounding area and the nearby Class I area due to SCC's proposed modification. The nearest Class I area is the Okefenokee National Wilderness Area (NWA), located in the Okefenokee National Wildlife Refuge located approximately 60 kilometers (km) northwest of the SCC plant. The next closest Class I area to SCC is Wolf Island, located approximately 98 km north of SCC. Due to the distance from SCC, the Okefenokee Class I area would potentially receive much higher impacts than Wolf Island. Therefore, only the Okefenokee NWA is addressed in this analysis.

The analysis will demonstrate that the increase in impacts due to the proposed increase in emissions is extremely low. Regardless of the existing conditions in the vicinity of the site or in the Class I areas, the proposed project will not cause any adverse impacts due to the predicted low impacts upon these areas.

#### 7.2 SOIL, VEGETATION, AND AORV ANALYSIS METHODOLOGY

In the foregoing analysis, the maximum air quality impacts predicted to occur in the vicinity of the SCC plant and in the Class I area due to the increase in emissions are used. The air modeling analysis which predicts the impacts on these areas was presented in Section 6.0.

The analysis involved predicting worst-case maximum short- and long-term concentrations of pollutants in the vicinity of the plant and in the Class I areas and comparing the maximum predicted concentrations to lowest observed effect levels for AQRVs or analogous organisms. In conducting the assessment, several assumptions were made as to how pollutants interact with the different matrices, i.e., vegetation, soils, wildlife, and aquatic environment.

A screening approach was used to evaluate potential effects which compared the maximum predicted ambient concentrations of air pollutants of concern with effect threshold limits for both vegetation and wildlife as reported in the scientific literature. A literature search was conducted which specifically addressed the effects of air contaminants on plant species reported to occur in the vicinity of the plant and the Class I area. It was recognized that effects threshold information is not available for all species found in the Okefenokee NWA, although studies have been performed on a few of the common species and on other similar species which can be used as models. In conducting the assessment, both direct (fumigation) and indirect (soil accumulation/uptake) exposures were considered for flora, and direct exposure (inhalation) was considered for wildlife.

# 7.3 IMPACTS TO SOILS, VEGETATION, AND VISIBILITY IN VICINITY OF THE SCC PLANT

# 7.3.1 PREDICTED AIR QUALITY IMPACTS

The results of the ambient air quality modeling for the proposed SCC modification, in the vicinity of the plant, were presented in Table 6-9. Maximum predicted concentrations were presented for the annual, 24-hour, 8-hour, 3-hour, and 1-hour averaging times.

### 7.3.2 IMPACTS TO SOILS

Soils in the vicinity of the SCC site consist primarily of tidal lands and poorly drained sands with organic pans. The tidal lands occur along the coast, and consist of mucky fine sand to dark-gray fine sand overlying gray fine sand, mixed with broken and whole shells. These soils will not be affected by NO<sub>2</sub> concentrations resulting from facility emissions, because both the underlying substrate and the sea spray from the nearby St. Johns river are neutral to alkaline and would neutralize any acidifying effects of NO<sub>2</sub> deposition.

The poorly drained sands are already strongly acidic. Normal liming practices currently used on soils in the vicinity of SCC by agricultural interests will effectively mitigate the small effects of any increased NO<sub>2</sub> deposition resulting from the increased NO<sub>2</sub> emissions from the proposed project.

Based on the small ambient NO<sub>2</sub> impacts due to the proposed project (1.23  $\mu$ g/m³), annual average, and the low existing air quality (28 $\mu$ g/m³) compared to the AAQS, no adverse impacts to soils is expected.

#### 7.3.3 IMPACTS TO VEGETATION

# **Vegetation Analysis**

In general, the effects of air pollutants on vegetation occur primarily from SO<sub>2</sub>, NO<sub>2</sub>, O<sub>3</sub>, and PM. Effects from minor air contaminants such as fluoride, chlorine, hydrogen chloride, ethylene, ammonia, hydrogen sulfide, CO, and pesticides have also been reported in the literature. The effects of air pollutants are dependent both on the concentration of the contaminant and the duration of the exposure. The term "injury," as opposed to damage, is commonly used to describe all plant responses to air contaminants and will be used in the context of this analysis. Air contaminants are thought to interact primarily with plant foliage which is considered to be the major pathway of exposure. For purposes of this analysis, it was assumed that 100 percent of each air contaminant of concern is accessible to the plants.

Injury to vegetation from exposure to various levels or air contaminants can be termed acute, physiological, or chronic. Acute injury occurs as a result of a short-term exposure to a high contaminant concentration and is typically manifested by visible injury symptoms ranging from chlorosis (discoloration) to necrosis (dead areas). Physiological or latent injury occurs as the result of a long-term exposure to contaminant concentrations below that which results in acute injury symptoms. Chronic injury results from repeated exposure to low concentrations over extended periods of time, often without any visible symptoms, but with some effect on the overall growth and productivity of the plant. In this assessment, 100 percent of the particular air pollutant in the ambient air was assumed to interact with the vegetation. This is a conservative approach.

A review of the literature indicates great variability in  $NO_2$  dose-response relationship in vegetation. Acute  $NO_2$  injury symptoms are manifested as water-soaked lesions, which first appear on the upper surface, followed by rapid tissue collapse. Low-concentration, long-term exposures as frequently encountered in polluted atmospheres often do not induce the lesions associated with acute exposures but may still result in some growth suppression. Citrus trees exposed to  $470 \mu g/m^3$  of  $NO_2$  for 290 days showed injury (Thompson *et al.*, 1970). Sphagnum exposed for 18 months at an average concentration of  $11.7 \mu g/m^3$  showed reduced growth (Press *et al.*, 1986)

The maximum ground-level NO<sub>2</sub> concentrations (1-hour and annual average) predicted to occur in the vicinity of the plant during the operation of the proposed project are 115  $\mu$ g/m³ and 39  $\mu$ g/m³,

respectively (see Tables 6-9 and 6-12). These maximum predicted concentrations are well below reported effects levels.

#### 7.3.4 IMPACTS UPON VISIBILITY

All air emission sources affected by the proposed modification are existing sources. No increase in permitted emissions is requested, although actual emissions are predicted to increase slightly. All these sources are in compliance with opacity regulations and should remain in compliance after the modification. As a result, no adverse impacts upon visibility are expected.

#### 7.3.5 IMPACTS DUE TO ASSOCIATED POPULATION GROWTH

There will be no increase in the number of workers during the construction period. There will be no significant increase in permanent employment at SCC as a result of the proposed project. Therefore, there will be no anticipated permanent impacts on air quality caused by associated population growth.

# 7.4 CLASS I AREA IMPACT ANALYSIS

# 7.4.1 DEFINITION OF AQRVS AND CRITERIA APPLIED TO OKEFENOKEE NWA

The Okefenokee NWA is classified as a Class I area by the U.S. Fish and Wildlife Service (USFWS) for purposes of PSD new source review. The U.S. Department of the Interior (National Park Service) in 1978 administratively defined air quality related values (AQRVs) for such areas as being:

All those values possessed by an area except those that are not affected by changes in air quality and include all those assets of an area whose vitality, significance, or integrity is dependent in some way upon the air environment. These values include visibility and those scenic, cultural, biological, and recreational resources of an area that are affected by air quality.

Important attributes of an area are those values or assets that make an area significant as a natural monument, preserve, or primitive area. They are the assets that are to be preserved if the area is to achieve the purposes for which it was set aside. (Federal Register, 1978)

# 7.4.2 AQRVS OF OKEFENOKEE NWA

To date, specific AQRVs other than visibility have not been defined by USFWS for the Okefenokee NWA (Ellen Porter, USFWS, Denver, CO, pers. comm., 1994). For this analysis, therefore, the

AQRVs of this Class I area are defined as those important attributes of the Okefenokee NWA which are dependent upon the air environment, including water, soil, vegetation resources, and wildlife resources. Important aquatic, vegetation, and wildlife attributes of these areas which make the Okefenokee NWA significant are presented in Table 7-1. All terrestrial vegetation, including threatened and endangered plant species of the Okefenokee NWA, are dependent upon the air environment and are considered AQRVs. Some terrestrial wildlife and endangered and threatened wildlife are also considered AQRVs for Okefenokee NWA. Threatened and endangered species associated with terrestrial habitats of the Okefenokee NWA are listed in Table 7-2.

# 7.4.3 REPORTED AIR QUALITY EFFECTS ON OKEFENOKEE NWA

No ecological effects to the attributes of the Okefenokee NWA have been reported to date (Sara Brown, USFWS, Folkston, GA; Robin Goodlow, USFWS, Brunswick, GA; and Ellen Porter, USFWS, Denver, CO, pers. comm., 1994). In 1991, a lichen study was completed (Wetmore, 1991) which did not find any damage to lichens from SO<sub>2</sub>. The trace element content including Cd, Cr, and Pb in six species of lichens and Spanish moss were considered normal. The range in concentrations of these trace metals found in lichens and Spanish moss from the Okefenokee National Wildlife Refuge is presented in Table 7-3. In addition, the general concern regarding potential effects of mercury (Hg) were raised. (Ellen Porter, USFWS, Denver, CO, pers. comm., 1994). The reported general effects on aquatic, vegetation, and wildlife resources from significant degradation in air quality are described in Table 7-4.

# 7.4.4 PREDICTED AIR QUALITY IMPACTS IN THE CLASS I AREA

The results of the air quality modeling for the increase in emissions due to the SCC modification are presented in Table 7-5. Predicted air quality concentrations are presented for Okefenokee NWA for the annual, 24-hour, 8-hour, 3-hour, and 1-hour averaging times. These concentrations reflect only the increase in emissions due to the proposed project.

# 7.4.5 VEGETATION AQRVS ANALYSIS

In general, the effects of air pollutants on vegetation occur primarily from SO<sub>2</sub>, NO<sub>2</sub>, O<sub>3</sub>, and PM. Effects from minor air contaminants such as fluoride, chlorine, hydrogen chloride, ethylene, ammonia, hydrogen sulfide, CO, and pesticides have been also reported in the literature. The effects of air pollutants are dependent both on the concentration of the contaminant and the duration

of the exposure. The term "injury," as opposed to damage, is commonly used to describe all plant responses to air contaminants and will be used in the context of this analysis. Air contaminants are thought to interact primarily with plant foliage which is considered to be the major pathway of exposure. For purposes of this analysis, it was assumed that 100 percent of each air contaminant of concern is accessible to the plants.

Injury to vegetation from exposure to various levels or air contaminants can be termed acute, physiological, or chronic. Acute injury occurs as a result of a short-term exposure to a high contaminant concentration and is typically manifested by visible injury symptoms ranging from chlorosis (discoloration) to necrosis (dead areas). Physiological or latent injury occurs as the result of a long-term exposure to contaminant concentrations below that which results in acute injury symptoms. Chronic injury results from repeated exposure to low concentrations over extended periods of time, often without any visible symptoms, but with some effect on the overall growth and productivity of the plant. In this assessment, 100 percent of the particular air pollutant in the ambient air was assumed to interact with the vegetation. This is a conservative approach.

A review of the literature indicates great variability in  $NO_x$  dose-response relationship in vegetation. Acute  $NO_2$  injury symptoms are manifested as water-soaked lesions, which first appear on the upper surface, followed by rapid tissue collapse. Low-concentration, long-term exposures as frequently encountered in polluted atmospheres often do not induce the lesions associated with acute exposures but may still result in some growth suppression. Citrus trees exposed to  $470 \mu g/m^3$  for 290 days showed injury (Thompson *et al.*, 1970). Sphagnum moss exposed for 18 months at an average concentration of  $11.7 \mu g/m^3$  showed reduced growth (Press *et al.*, 1986).

The maximum ground-level  $NO_2$  concentrations (1-hour and annual average) predicted to occur at the Class I area boundary due to the increase in emissions are 1.7 and 0.009  $\mu$ g/m³ respectively. These values are well below reported effect concentrations and no effects are predicted to occur.

# 7.4.6 SOILS AQRV ANALYSIS

Air contaminants can affect soils through fumigation by gaseous forms, accumulation of compounds transformed from the gaseous state, or by the direct deposition of particulate matter or particulate matter to which certain contaminants are absorbed. Gaseous fumigation of soils does not directly

affect the soil but rather the organisms found in the soil. Concentrations several orders of magnitude higher than the predicted value are required before any adverse effects from fumigation are observed. It is more likely that effects on soils and the organisms (plants and animals) found in the soils could occur from the deposition of trace elements over the life of the project. Thus, this analysis of effects on soils specifically addresses the deposition of trace elements and potential pathways for movements into the vegetation.

The maximum predicted NO<sub>2</sub> concentration at the Class I Area due to the proposed project is  $0.009 \ \mu g/m^3$ , annual average. This impact is consider negligible, and no effects are predicted.

# 7.4.7 WILDLIFE AQRV ANALYSIS

The predicted NO<sub>2</sub> concentrations are also well below the lowest observed effects levels in animals (Table 7-6) and pose no risk to wildlife AQRVs in the Class I area. Because predicted levels are below those known to cause effects to vegetation, there is also no risk to their habitat.

#### 7.4.8 VISIBILITY IMPACTS

The visibility impacts of the proposed boiler's maximum future emissions are provided in Table 7-7. The modeling results, using the VISCREEN model, indicate that the maximum visibility impacts caused by the future plant's total emissions do not exceed the screening criteria inside or outside the Class I area. As a result, the proposed project is predicted to have no adverse effects to visibility in the Class I area.

# **7.4.9 SUMMARY**

In summary, it is apparent that very large margins of safety exist for all matrices examined with respect to the effects of the predicted increase in emissions on the Class I areas. No significant adverse effects will occur to the AQRVs in the Okefenokee NWA due to the modification of the SCC plant.

Table 7-1. Important Aquatic, Vegetational, and Wildlife Resource Attributes or AQRVs of Okefenokee NWA Dependent Upon the Air Environment

Attribute	Location		
Aquatic			
Blackwater rivers, ponds, sloughs	Okefenokee NWA	-	
Vegetation			
Ecological communities including:			
Cypress wetlands	Okefenokee NWA		
Wet flatwoods	Okefenokee NWA		
Bay-shrub bogs	Okefenokee NWA		
Basin marshes	Okefenokee NWA		
Mixed hardwood swamp	Okefenokee NWA		
Unique ecological communities			
Old-growth cypress swamp	Okefenokee NWA		
Unique plants			
Threatened and endangered species Ephiphytic plants including orchids	Okefenokee NWA		
and bromeliads	Okefenokee NWA		
Air quality bioindicators - lichens	Okefenokee NWA		
Wildlife			
Birds, mammals, reptiles and amphibians	Okefenokee NWA		
Threatened and endangered species (see Table 7-3)	Okefenokee NWA		

Note: NWA = National Wilderness Area.

Source: KBN, 1995.

Table 7-2. Federal and State Listed Endangered and Threatened Animals in the Okefenokee NWA
Dependent Upon the Air Environment

	Designated Status			
Species	State*	USFWS <sup>b</sup>		
Florida Black Bear	S4	C2		
Arctic Peregrine Falcon	S1	•		
Bachman's Warbler	Е	E		
Bald Eagle	E	Е		
Piping Plover	S1/S2	T		
Red-Cockaded Woodpecker	Е	E		
Wood Stork	S2	E		
American Alligator	-	T(S/A)		
Eastern Indigo Snake	S3	T		

State (Georgia) Status:

E = endangered.

S1 = regionally endangered.

S2 = regionally threatened.

S3 = regionally of concern.

S4 = regionally apparently secure.

# b USFWS Status:

C2 = candidate for listing, with some evidence of vulnerability, but for which not enough data exist to support listing.

E = endangered.

T = threatened.

T(S/A) = threatened due to similarity of appearance.

Sources: U.S. Fish and Wildlife Service.

Georgia Freshwater Wetlands and Heritage Inventory Program.

Reported Representative Trace Metal Concentrations in Lichens and Spanish Moss in Okefenokee National Wildlife Refuge Table 7-3.

	Concentration (ppm dry weight)						
Species	Cd	Cr	Pb	Mn	Cu	Zn	
Lichens							
Usnea baileyi <sup>a</sup>	ND — 0.3	ND - 0.3	2.6 - 4.9	12.3 — 50.7	1.0 1.6	16.3 — 29.7	
Usnea mutabilisª	ND	0.2	4.9	55.1	1.8	20.7	
Parmelia rampoddensisª	ND — 0.6	0.3 — 0.6	4.7 — 10.0	8.0 — 88.0	1.4 — 3.2	21.9 — 31.6	
Parmelia tinctorumª	0.5	0.5	7.3	25.0	2.6	25.9	
Cladina substygia <sup>b</sup>	ND	0.2 — 0.6	1.9 — 2.3	7.4 — 12.0	0.9 — 1.1	9.1 — 10.7	
Cladina leporina <sup>b</sup>	ND	1.4 — 1.6	7.5 — 7.8	7.9 — 9.2	1.4 — 1.5	11.4 — 11.6	
Spanish Moss		·					
Tillandsia usneoides	ND 0.5	0.7 — 1.0	4.6 — 8.4	37.3 — 284.3	2.4 — 3.7	17.3 — 31.4	

Source: Wetmore, 1991.

<sup>&</sup>lt;sup>a</sup> Range in means.
<sup>b</sup> Range in single values.

Table 7-4. Reported General Effects on Aquatic, Vegetation, and Wildlife Resources From Significant Degradation in Air Quality

Attribute	Potential Effects and Associated Air Quality Change			
Aquatic Resources	Acidification of waters and subsequent changes (loss and replacement) of ecological components; sensitive systems have low buffering capacity			
Vegetation Resources	Most common effects include reduced growth, injury, and species replacement; species show specific sensitivity			
Wildlife Resources	Potential effects include avoidance and increased body burdens of contaminants			

Source: KBN, 1995.

Table 7-5. Predicted Increase in Maximum NO<sub>2</sub> Concentrations at the Okefenokee Class I Area Due to the Proposed Modification

Averaging Time	Predicted Concentration (µg/m³) <sup>a</sup>
Highest 1-hour	1.7
Highest 3-hour	0.8
Highest 8-hour	0.5
Highest 24-hour	0.2
Annual	0.009

<sup>&</sup>lt;sup>a</sup> Highest predicted impact.

Table 7-6. Lowest Observed Effect Levels of  $NO_2$  in Animals

Pollutant	Reported Effect	Concentration (μg/m³)	Exposure		
Nitrogen Dioxide	Respiratory stress in mice	1,917	3 hours		
	Respiratory stress in guinea pigs	95 to 950	8 hr/day for <sup>a</sup> 122 days		

<sup>&</sup>lt;sup>a</sup> Used to compare as a range between 3-hour and 24-hour averaging times.

Source: Adapted from Newman (1980) and Newman and Schreiber (1988).

Table 7-7. Visual Effects Screening Analysis for Source: STONE CONTAINER CORP - JACKSONVILLE Class I Area: OKEFENOKEE NWA

# Level-1 Screening \*\*\*

# Input Emissions for

Particulates	4.35 LB/HR
NOx (as NO2)	104.80 LB/HR
Primary NO2	.00 LB /HR
Soot	.00 LB/HR
Primary SO4	.00 LB/HR

# \*\*\*\* Default Particle Characteristics Assumed

# Transport Scenario Specifications:

Background Ozone:	.04 ppm
Background Visual Range:	65.00 km
Source-Observer Distance:	61.00 km
Min. Source-Class I Distance:	61.00 km
Max. Source-Class I Distance:	80.00 km
Plume-Source-Observer Angle:	11.25 degrees
Stability: 6	

Wind Speed:

1.00 m/s

# RESULTS

# Asterisks (\*) indicate plume impacts that exceed screening criteria

# Maximum Visual Impacts INSIDE Class I Area Screening Criteria ARE NOT Exceeded

					Delta E		Contrast	
					=====		=======	
Backgrnd	Theta	Azi	Distance	Alpha	Crit	Plume	Crit	Plume
=====	===	===	====	===	===	===	===	====
SKY	10.	84.	61.0	84.	2.00	.725.	05	002
SKY	140.	84.	61.0	84.	2.00	.303.	05	004

# Maximum Visual Impacts OUTSIDE Class I Area Screening Criteria ARE NOT Exceeded

					Delta E		Contrast	
					======		=======	
Backgrnd	Theta	Azi	Distance	Alpha	Crit	Plume	Crit	Plume
=====	===	===	====	===	===	===	===	====
SKY	10.	35.	48.4	134.	2.00	.860	.05	003
SKY	140.	35.	48.4	134.	2.00	.355	.05	005

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(Page 2 of 2)

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# APPENDIX A

**EXISTING SCC PERMITS** 



# Department of Environmental Protection

Lawton Chiles Governor Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Virginia B. Wetherell Secretary

December 8, 1995

CERTIFIED MAIL - RETURN RECEIPT REQUESTED

Mr. John L. West Stone Container Corporation 9469 East Port Road Jacksonville, Florida 32229

Dear Mr. West:

RE: Request for Permit Modification Stone Container Corporation (Formerly Seminole Kraft Corp.) AC16-222359, PSD-FL-198 (A); Duval County

The Department received your requests of June 15 and August 9, 1995, to modify the above referenced construction permit by maximizing steam generation from the three boilers, and increasing the hourly and annual nitrogen oxides ( $NO_X$ ) emission rate for each boiler based on 0.2 lb/MMBtu and the maximum allowable heat input rate. The modification, which also extends the expiration date of the construction permit referenced above, is as follows:

Permit No. AC16-222359, PSD-FL-198 (A), Stone Container Corporation.

Current Expiration Date: August 31, 1995

New Expiration Date: April 1, 1996

The Department is also modifying the specific conditions as follows:

- The construction and operation of these sources shall be in accordance with the capacities stated in the Revised Technical-Evaluation-and-Preliminary-Betermination application dated June 1995.
- 2. The packaged package boilers may be operated continuously (8760 hrs/yr).
- 3. The maximum heat input rate to each boiler shall neither exceed 174.7 MMBtu/hr while firing natural gas nor 164.5 MMBtu/hr while firing No. 2 fuel oil.

Mr. John L. West December 8, 1995 Page Two

- 4. In accordance with the terms of the Cedar Bay Cogeneration Project (CBCP) site certification, Stone Container

  Corporation (SCC) is limited to producing 375,000 lbs/hr of steam from its three package boilers.
- 5. The maximum allowable NO<sub>X</sub> emissions shall not exceed 0.2 lb/MMBtu, 23-6 34.94 lbs/hr and 103-4 153.1 tons/yr per boiler. The total NO<sub>X</sub> emissions from the three package boilers, in accordance with the terms of the CBCP site certification, shall not exceed 310 tons per year.
- 4. 6. The three packaged package boilers are permitted to fire both natural gas and No. 2 fuel oil, with the primary fuel being natural gas. The sulfur content of the No. 2 fuel oil shall not exceed 0.05 percent, by weight. Any delivery of No. 2 fuel oil shall be accompanied by a laboratory analysis quantifying the density and percent sulfur, by weight. Annual SO<sub>2</sub> emissions from No. 2 fuel oil firing, totaling all three boilers, shall not exceed 25 tons/year. In the event that the ceiling for SO2 is expected to be exceeded due to unavailability of natural gas caused by factors beyond the control of 6Ke SCC, 6Ke SCC shall notify the Department that it anticipates exceeding the ceiling as provided herein; and, the emissions of SO<sub>2</sub> during the period of such curtailment shall not be counted against the yearly emissions ceiling of 25 tons unless administrative proceedings result in a finding that the exceedance was within SKC's control. event shall the total annual emissions of SO2 from the three steam boilers exceed 41 tons/year. The notice shall include a statement or reasons for the request and supporting documentation, and shall be published by SKE SCC, without supporting documents, in a newspaper of general circulation in Jacksonville, Florida, as defined in Section 403.5115(2), The filing and publication of the notice no later than 7 days following the date of exceedance, shall preclude any finding of violation by the Department until final disposition of any administrative proceedings.
- 5. 7. Visible emissions (VE) shall not exceed 5 percent(%) opacity during natural gas firing and 10% opacity during fuel oil firing.
- 6. 8. In accordance with the requirements of 40 CFR 60.48<u>b</u>(b), a <u>continuous emission</u> monitoring system (CEMs) for nitrogen oxides shall be installed, operated, and maintained. Also,

Mr. John L. West December 8, 1995 Page Three

the natural gas, fuel oil and steam flows (both from the packaged package boilers and from the CBCP facility) shall be metered and continuously recorded. The data shall be logged daily and maintained so that it can be provided to the Department upon request.

- 7. 9. Before this construction permit expires, each packaged package boiler shall be tested and monitored for compliance with the emission limits in Specific Conditions No. 5, 6 and 7. Compliance tests for NO<sub>X</sub> shall be conducted in accordance with 40 CFR 60.46b(e)(3)(4). Compliance with SO<sub>2</sub> limits shall be in accordance with 40 CFR 60.49b(r), and a stoichiometric quantification for SO<sub>2</sub> emissions shall be utilized using the actual density and sulfur weight percent and the quantity of fuel oil fired monthly. Compliance with visible emission limits shall be demonstrated initially and annually in accordance with EPA Method 9.
- 8. 10. The Department's Northeast District office and the RESD (City of Jacksonville's Regulatory and Environmental Services Department) office shall be notified at least 15 days prior to the compliance tests. Compliance test results shall be submitted to the Department's Northeast District and Bureau of Air Regulation offices and the RESD office within 45 days after completion of the tests. Sampling facilities, methods and reporting shall be in accordance with 40 CFR 60.49b, F.A.C Rule-17-2-700 Chapter 62-297 and 40 CFR 60, Appendix A.
- 9. 11. The following Seminole-Kraft-Corporation-(SKC) SCC sources shall be permanently shut down and made incapable of operation: the No. 1 PB (power boiler), the No. 2 PB, the No. 3 PB, the No. 1 BB (bark boiler) and the No. 2 BB; and, SKC SCC shall turn in their operation permits to the Department's Bureau of Air Regulation, within 30 days of written confirmation by the Department of the successful completion of the initial compliance tests on the Cedar Bay Cogeneration Plant's boilers. The RESD office shall be specifically informed in writing within thirty days after each individual shut down of the above referenced equipment.
- 10. 12. The permittee, for good cause, may request that this construction permit be extended. Such a request shall be submitted to the Department's Bureau of Air Regulation prior to 60 days before the expiration of the permit. (Rule 17 62-4.090 F.A.C.)
- 11. 13. If Florida is granted interim or full approval for the Title V operation permit program prior to January 1, 1996, this condition is negated. An application for an operation

Mr. John L. West December 8, 1995 Page Four

permit must be submitted to the Department's Northeast District office and the RESD office at least 90 days prior to the expiration date of this construction permit. To properly apply for an operation permit, the applicant shall submit the appropriate application form, fee, certification that construction was completed noting any deviations from the conditions in the construction permit, and compliance test reports as required by this permit. (Rules 17 62-4.055 and 17 62-4.220, F.A.C.)

12. 14. Pursuant to 40 CFR 60.49b(r), quarterly reports shall be submitted to the RESD office (i.e., Administrator) certifying that only very low sulfur oil (i.e., ≤0.05% sulfur, by weight) meeting this definition was combusted in the affected facility during the preceding quarter. The firing of any fuel oil and its associated SO<sub>2</sub> emissions shall be quantified on a monthly and per boiler basis and submitted to the RESD office by the end of the month following the end of each quarter. The quarters are defined as January-March, April-June, July-September and October-December; also, and per boiler, the final quarterly report shall include the total amount of the fuel oil fired and the quantified associated SO<sub>2</sub> emissions from for the year.

A copy of this letter shall be attached to the above mentioned permit, AC16-222359, PSD-FL-198 (A), and shall become a part of the permit.

Sincerely,

Howard L. Rhodes, Director Division of Air Resources Management

HLR/sa/t

cc: C. Kirts, NED

- S. Pace, RESD
- J. Harper, EPA
- J. Bunyak, NPS
- S. Shirley, OHF&C

# Additional Distribution List

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# Florida Department of

# Environmental Protection

Lawton Chiles Governor

Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Virginia B. Weitherell Secretary

PERMITTEE:

Seminole Kraft Corporation 9469 East Port Road Jacksonville, Florida 32229 Permit Number: AC 16-222359

PSD-FL-198

Expiration Date: April 30, 1995

County: Duval

Latitude/Longitude: 30°25'15"N - 81°36'00"W

Three Packaged Steam Project:

Boilers

This permit is issued under the provisions of Chapter 403, Florida Statutes, and Florida Administrative Code Chapters 17-210 through 297 and 17-4. The above named permittee is hereby authorized to perform the work or operate the facility shown on the application and approved drawings, plans, and other documents attached hereto or on file with the Department of Environmental Protection (Department) and made a part hereof and specifically described as follows:

For the construction of three 125,000 lbs/hr packaged process steam boilers. The facility is located at 9469 East Port Road, Jacksonville, Duval County, Florida. UTM coordinates of the site are: Zone 17, 441.8 km E and 3,365.6 km N.

Emissions shall be controlled by using clean fuels and good combustion practices.

The source shall be constructed in accordance with the permit application, plans, documents, amendments and drawings, except as otherwise noted in the General and Specific Conditions.

#### Attachments are listed below:

- Letter (with proposed gas contract) from Oertel to Pennington (12/3/92).
- 2. Letter from KBN to the Department (12/9/92).
- Letter from Georgia DNR to the Department (12/10/92).
- Letter from KBN to the Department (12/22/92).
- Incompleteness letter from the Department to SKC (12/23/92).
- Letter from KBN to the Department (12/23/92).
- Second Incompleteness letter from the Department to SKC (1/5/93).
- Letter from KBN to the Department (1/8/93).
- Letter from EPA to the Department (1/15/93).
- 10. Letter from Oertel to the Department (1/19/93).
- 11. Third Incompleteness letter from the Department to SKC (1/25/93).
- 12. Letter from Oertel to the Department (1/29/93). 13. Letter from Oertel to the Department (1/29/93).
- 14. Completeness letter from the Department to SKC (2/10/93).
- 15. Technical Evaluation and Preliminary Determination (TE&PD) mailed 4/2/93.

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PERMITTEE: Seminole Kraft Corp. Permit Number:

AC 16-222359

PSD-FL-198

Expiration Date: April 30, 1995

#### Attachments cont.:

Mr. Ronald L. Roberson's letter received 4/20/93.

17. Mr. Brian L. Beals's letter received 4/22/93.

Revised TE&PD mailed 4/21/93.

19. Public Notice received 5/7/93 (incomplete).

20. Mr. James W. Pulliam, Jr.'s letter received 5/21/93.

21. Public Notice received 5/27/93.

- 22. Ms. Jewell A. Harper's letter received 6/11/93.
- 23. Final Determination dated 7/7/93.

### GENERAL CONDITIONS:

- The terms, conditions, requirements, limitations, and restrictions set forth in this permit are "Permit Conditions" and are binding and enforceable pursuant to Sections 403.161, 403.727, or 403.859 through 403.861, Florida Statutes (F.S.). The permittee is placed on notice that the Department will review this permit periodically and may initiate enforcement action for any violation of these conditions.
- This permit is valid only for the specific processes and operations applied for and indicated in the approved drawings or exhibits. And unauthorized deviation from the approved drawings, exhibits, si ifications, or conditions of this permit may constitute grounds for revocation and enforcement action by the Department.
- As provided in Subsections 403.087(6) and 403.722(5), F.S., the issuance of this permit does not convey any vested rights or any exclusive privileges. Neither does it authorize any injury to public or private property or any invasion of personal rights, nor any infringement of federal, state or local laws or regulations. This permit is not a waiver of or approval of any other Department permit that may be required for other aspects of the total project which are not addressed in the permit.
- This permit conveys no title to land or water, does not constitute State recognition or acknowledgement of title, and does not constitute authority for the use of submerged lands unless herein provided and the necessary title or leasehold interests have been obtained from the State. Only the Trustees of the Internal Improvement Trust Fund may express State opinion as to title.
- This permit does not relieve the permittee from liability for harm or injury to human health or welfare, animal, or plant life, or property caused by the construction or operation of this permitted source, or from penalties therefore; nor does it allow the permittee to cause pollution in contravention of F.S. and Department rules, unless specifically authorized by an order from the Department.

PERMITTEE: Seminole Kraft Corp. Permit Number: AC 16-222359

PSD-FL-198

Expiration Date: April 30, 1995

#### GENERAL CONDITIONS:

6. The permittee shall properly operate and maintain the facility and systems of treatment and control (and related appurtenances) that are installed or used by the permittee to achieve compliance with the conditions of this permit, as required by Department rules. This provision includes the operation of backup or auxiliary facilities or similar systems when necessary to achieve compliance with the conditions of the permit and when required by Department rules.

- 7. The permittee, by accepting this permit, specifically agrees to allow authorized Department personnel, upon presentation of credentials or other documents as may be required by law and at a reasonable time, access to the premises, where the permitted activity is located or conducted to:
  - a. Have access to and copy any records that must be kept under the conditions of the permit;
  - b. Inspect the facility, equipment, practices, or operations regulated or required under this permit; and,
  - c. Sample or monitor any substances or parameters at any location reasonably necessary to assure compliance with this permit or Department rules.

Reasonable time may depend on the nature of the concern being investigated.

- 8. If, for any reason, the permittee does not comply with or will be unable to comply with any condition or limitation specified in this permit, the permittee shall immediately provide the Department with the following information:
  - a. a description of and cause of non-compliance; and,
  - b. the period of noncompliance, including dates and times; or, if not corrected, the anticipated time the non-compliance is expected to continue, and steps being taken to reduce, eliminate, and prevent recurrence of the non-compliance.

The permittee shall be responsible for any and all damages which may result and may be subject to enforcement action by the Department for penalties or for revocation of this permit.

9. In accepting this permit, the permittee understands and agrees that all records, notes, monitoring data and other information relating to the construction or operation of this permitted source

PERMITTEE: Seminole Kraft Corp. Permit Number: AC 16-222359 PSD-FL-198

Expiration Date: April 30, 1995

#### GENERAL CONDITIONS:

which are submitted to the Department may be used by the Department as evidence in any enforcement case involving the permitted source arising under the F.S. or Department rules, except where such use is prescribed by Sections 403.73 and 403.111, F.S. Such evidence shall only be used to the extent it is consistent with the Florida Rules of Civil Procedure and appropriate evidentiary rules.

- 10. The permittee agrees to comply with changes in Department rules and F.S. after a reasonable time for compliance, provided, however, the permittee does not waive any other rights granted by F.S. or Department rules.
- 11. This permit is transferable only upon Department approval in accordance with Florida Administrative Code (F.A.C.) Rules 17-4.120 and 17-730.300, as applicable. The permittee shall be liable for any non-compliance of the permitted activity until the transfer is approved by the Department.
- 12. This permit or a copy thereof shall be kept at the work site of the permitted activity.
- 13: This permit also constitutes:

  - (x) Determination of Prevention of Significant Deterioration; and,
  - (x) Compliance with New Source Performance Standards (NSPS).
- 14. The permittee shall comply with the following:
  - a. Upon request, the permittee shall furnish all records and plans required under Department rules. During enforcement actions, the retention period for all records will be extended automatically unless otherwise stipulated by the Department.
  - b. The permittee shall hold at the facility or other location designated by this permit records of all monitoring information (including all calibration and maintenance records and all original strip chart recordings for continuous monitoring instrumentation) required by the permit, copies of all reports required by this permit, and records of all data used to complete the application for this permit. These materials shall be retained at least three years from the date of the sample, measurement, report, or application unless otherwise specified by Department rule.

PERMITTEE: Seminole Kraft Corp.

Permit Number: AC 16-222359

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Expiration Date: April 30, 1995

c. Records of monitoring information shall include:

- the date, exact place, and time of sampling or measurements;
- the person responsible for performing the sampling or measurements;

- the dates analyses were performed;

- the person responsible for performing the analyses;
- the analytical techniques or methods used; and,
- the results of such analyses.

15. When requested by the Department, the permittee shall within a reasonable time furnish any information required by law which is needed to determine compliance with the permit. If the permittee becomes aware that relevant facts were not submitted or were incorrect in the permit application or in any report to the Department, such facts or information shall be corrected promptly.

#### SPECIFIC CONDITIONS:

- 1. The construction and operation of these sources shall be in accordance with the capacities stated in the Revised Technical Evaluation and Preliminary Determination.
- 2. The packaged boilers may be operated continuously (8760 hrs/yr).
- 3. The maximum allowable NOx emissions shall not exceed 0.2 lb/MMBtu, 23.6 lbs/hr, and 103.4 tons/yr per boiler.
- The three packaged boilers are permitted to fire both natural gas and No. 2 fuel oil, with the primary fuel being natural gas. The sulfur content of the No. 2 fuel oil shall not exceed 0.05 percent, by weight. Any delivery of No. 2 fuel oil shall be accompanied by a laboratory analysis quantifying the density and percent sulfur, by weight. Annual SO2 emissions from No. 2 fuel oil firing, total all three boilers, shall not exceed 25 tons/year. In the event that the ceiling for SO2 is expected to be exceeded due to unavailability of natural gas caused by factors beyond the control of SKC, SKC shall notify the Department that it anticipates exceeding the ceiling as provided herein; and, the emissions of SO2 during the period of such curtailment shall not be counted against the yearly emissions ceiling of 25 tons unless administrative proceedings result in a finding that the exceedance was within SKC's control. In no event shall the total annual emissions of SO2 from the three steam boilers exceed 41 tons/year. The notice shall include a statement or reasons for the request and supporting documentation, and shall be published by SKC, without supporting documents, in a newspaper of general circulation in Jacksonville,

PERMITTEE: Seminole Kraft Corp.

Permit Number: AC 16-222359 PSD-FL-198

Expiration Date: April 30, 1995

#### SPECIFIC CONDITIONS:

Florida, as defined in Section 403.5115(2), F.S. The filing and publication of the notice no later than 7 days following the date of exceedance, shall preclude any finding of violation by the Department until final disposition of any administrative proceedings.

- 5. Visible emissions (VE) shall not exceed 5% opacity during natural gas firing and 10% opacity during fuel oil firing.
- 6. In accordance with requirements of 40 CFR 60.48(b), a monitoring system (CEMS) for nitrogen oxides shall be installed, operated, and maintained. Also, the natural gas, fuel oil and steam flows (both from the packaged boilers and from the CBCP facility) shall be metered and continuously recorded. The data shall be logged daily and maintained so that it can be provided to the Department upon request.
- 7. Before this construction permit expires, each packaged boiler shall be tested and monitored for compliance with the emission limits in Specific Conditions No. 4, 5, and 6. Compliance tests for NOx shall be conducted in accordance with 40 CFR 60.46b(e)(3). Compliance with SO<sub>2</sub> limits shall be in accordance with 40 CFR 60.49b(r); and, a stoichiometric quantification for SO<sub>2</sub> emissions shall be utilized using the actual density and sulfur weight percent and the quantity of fuel oil fired monthly. Compliance with visible emission limits shall be demonstrated initially and annually in accordance with EPA Method 9.
- 8. The Department's Northeast District office and the RESD (City of Jacksonville's Regulatory and Environmental Services Department) office shall be notified at least 15 days prior to the compliance tests. Compliance test results shall be submitted to the Department's Northeast District and Bureau of Air Regulation offices and the RESD office within 45 days after completion of the tests. Sampling facilities, methods, and reporting shall be in accordance with 40 CFR 60.49b, F.A.C. Rule 17-2.700 and 40 CFR 60, Appendix A.
- 9. The following Seminole Kraft Corporation (SKC) sources shall be permanently shut down and made incapable of operation: the No. 1 PB (power boiler), the No. 2 PB, the No. 3 PB, the No. 1 BB (bark boiler), and the No. 2 BB; and, SKC shall turn in their operation permits to the Department's Bureau of Air Regulation, within 30 days of written confirmation by the Department of the successful completion of the initial compliance tests on the Cedar Bay Cogeneration Plant's boilers. The RESD office shall be specifically informed in writing within thirty days after each individual shut down of the above referenced equipment.

PERMITTEE: Seminole Kraft Corp. Permit Number: AC 16-222359

PSD-FL-198

Expiration Date: April 30, 1995

### SPECIFIC CONDITIONS:

10. The permittee, for good cause, may request that this construction permit be extended. Such a request shall be submitted to the Department's Bureau of Air Regulation prior to 60 days before the expiration of the permit (F.A.C. Rule 17-4.090).

- 11. An application for an operation permit must be submitted to the Department's Northeast District office and the RESD office at least 90 days prior to the expiration date of this construction permit. To properly apply for an operation permit, the applicant shall submit the appropriate application form, fee, certification that construction was completed noting any deviations from the conditions in the construction permit, and compliance test reports as required by this permit (F.A.C. Rules 17-4.055 and 17-4.220).
- 12. Pursuant to 40 CFR 49b(r), quarterly reports shall be submitted to the RESD office (i.e., Administrator) certifying that only very low sulfur oil (i.e.,  $\leq 0.05$ % sulfur, by weight) meeting this definition was combusted in the affected facility during the preceding quarter. The firing of any fuel oil and its associated  $SO_2$  emissions shall be quantified on a monthly and per boiler basis and submitted to the RESD office by the end of the month following the end of each quarter. The quarters are defined as January-March, April-June, July-September, and October-December; also, and per boiler, the final quarterly report shall include the total amount of the fuel oil fired and the quantified associated  $SO_2$  emissions from the year.

Issued this 7<sup>th</sup> day of **Tal**, 1993

STATE OF FLORIDA DEPARTMENT OF ENVIRONMENTAL PROTECTION

Virginia B. Wetherell, Secretary

Revised Best Available Control Technology (BACT) Determination

Seminole Kraft Corporation

Duval County

PSD-FL-198

AC 16-222359

The applicant proposes to install three packaged boilers at their recycled fiber paper mill facility in Jacksonville, Duval County, Florida. Each of the three boilers will be sized to provide up to 125,000 lbs/hr of process steam for Seminole Kraft Corporation's (SKC) paper machines. SKC will also receive process steam from the adjacent Cedar Bay Cogeneration Project (CBCP). According to terms of the CBCP Site Certification proceedings, SKC is to be limited to a total steam production of 640,000 lbs/hr which includes 380,000 lbs/hr imported from the CBCP facility. This leaves 260,000 lbs/hr to be produced by the three packaged boilers under normal operating conditions. During periods when CBCP is not operating or operating at reduced rates, SKC will be allowed to make up the difference between the 380,000 lbs/hr and the steam production level that CBCP provides. This is equivalent to a maximum firing rate of 524 MMBTU/hr for all three SKC packaged boilers when the CBCP facility is down.

### Date of Receipt of a Complete Application

February 10, 1993

### BACT Determination Requested by Applicant

SKC's application called for the firing of fuel oil on a full time or as needed basis since a firm natural gas contract had not been obtained at the time of filing. Consequently, the application required a BACT determination for SO2 and beryllium since these pollutants would be emitted in amounts exceeding PSD-significant levels. BACT was proposed by the applicant as firing fuel oil with a 0.5 percent maximum sulfur content (0.3 average). Since there are no specific control technologies for beryllium, an uncontrolled beryllium emission level was proposed.

#### BACT Determination by the Department

During initial permitting discussions with SKC, the Department of Environmental Protection (Department) indicated to them that BACT would require the use of natural gas as the primary fuel, if available. Subsequently, SKC obtained a natural gas contract.

Revised BACT Seminole Kraft Corp. Page Two

Therefore, the Department's determination of BACT is three packaged steam boilers being allowed to fire both natural gas and No. 2 fuel oil (maximum 0.05% sulfur, by weight), with the primary fuel being natural gas. Allowable emissions under normal operating conditions (i.e. 380,000 lbs/hr steam supplied by CBCP) are listed below for each boiler along with the limit basis:

<u>Pollutant</u>	<u>Emission Limits</u>	<u>Basis</u>
NO <sub>X</sub> SO <sub>2</sub>	23.6 lbs/hr and 103.4 tons/yr 25 tons/yr total-3 boilers*	Subpart D <sub>b</sub> (0.2 lb/mm BTU) BACT (≤0.05% S, by wt. #2 Fuel Oil)
VE VE	Natural Gas - 5% opacity No. 2 Fuel Oil - 10% opacity	BACT BACT

\* In the event that the ceiling for SO2 is expected to be exceeded due to unavailability of natural gas caused by factors beyond the control of SKC, SKC shall notify the Department that it anticipates exceeding the ceiling as provided herein; and, the emissions of SO $_{
m 2}$ during the period of such curtailment shall not be counted against the yearly emissions ceiling of 25 tons unless administrative proceedings result in a finding that the exceedance was within SKC's In no event shall the total annual emissions of SO2 from control. the three steam boilers exceed 41 tons/year. The notice shall include a statement or reasons for the request and supporting documentation, and shall be published by SKC, without supporting documents, in a newspaper of general circulation in Jacksonville, Florida, as defined in Section 403.5115(2), Florida Statutes. filing and publication of the notice no later than 7 days following the date of exceedance, shall preclude any finding of violation by the Department until final disposition of any administrative proceedings.

### BACT Determination Procedure

In accordance with Florida Administrative Code (F.A.C.) Rules 17-210 through 297, this BACT determination is based on the maximum degree of reduction of each pollutant emitted which the Department, on a case by case basis, taking into account energy, environmental and economic impacts, and other costs, determines is achievable through application of production processes and available control methods, systems and techniques. In addition, the regulations require that in making the BACT determination the Department shall give consideration to:

Revised BACT Seminole Kraft Corp. Page Three

- (a) Any Environmental Protection Agency determination of BACT pursuant to Section 169, and any emission limitation contained in 40 CFR Part 60 (Standards of Performance for New Stationary Sources) or 40 CFR Part 61 (National Emission Standards for Hazardous Air Pollutants).
- (b) All scientific, engineering and technical material and other information available to the Department.
- (c) The emission limiting standards or BACT determinations of any other State.
- (d) The social and economic impact of the application of such technology.

The EPA currently stresses that BACT should be determined using the "top-down" approach. The first step in this approach is to determine for the emission source in question the most stringent control available for a similar or identical source or source category. If it is shown that this level of control is technically or economically infeasible for the source in question, then the next most stringent level of control is determined and similarly evaluated. This process continues until the BACT level under consideration cannot be eliminated by any substantial or unique technical, environmental, or economic objections.

#### BACT Determination Rationale

BACT review for particulate emissions and sulfur-dioxide are required under F.A.C. Rule 17-296.406. Visible emissions may be regulated as a surrogate parameter for PM/PM<sub>10</sub> and have been established at 5% opacity for natural gas fired boilers (10% opacity for No. 2 fuel oil).

For SO<sub>2</sub> emissions from oil firing, only two alternatives exist that would result in stringent SO<sub>2</sub> emissions; using low sulfur content fuel oil or flue gas desulfurization (FGD). EPA has recognized that FGD technology is inappropriate to apply to these combustion units. Sludge would be generated that would have to be disposed of properly, and there would be greatly increased costs associated with the construction and operation of a FGD system. Finally, there is no information in the literature to indicate that FGD has ever been applied to burning distillate oil. This leaves the use of natural gas and low sulfur fuel oil as backup as the best option for this project. Due to the anticipated availability of very low sulfur oil by October 1993, the Department will require the use of No. 2 fuel oil with 0.05% sulfur by weight as BACT.

Revised BACT Seminole Kraft Corp. Page Four

### Details of the Analysis May be Obtained by Contacting:

Preston Lewis, P.E., BACT Coordinator Department of Environmental Protection Bureau of Air Regulation Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

Tallahassee, Florida 32399-2400

Recommended by:

C. H. Fancy, P.E., Chlief
Bureau of Air Regulation

Date

Pate

Approved by:

Virginia B. Wetherell, Secretary
Dept. of Environmental Protection

Date

Date

### APPENDIX B

**AP-42 EMISSION FACTORS** 

### 1.4 Natural Gas Combustion

### 1.4.1 General 1-2

Natural gas is one of the major fuels used throughout the country. It is used mainly for industrial process steam and heat production; for residential and commercial space heating; and for electric power generation. Natural gas consists of a high percentage of methane (generally above 85 percent) and varying amounts of ethane, propane, butane, and inerts (typically nitrogen, carbon dioxide, and helium). Gas processing plants are required for the recovery of liquefiable constituents and removal of hydrogen sulfide before the gas is used (see Section 5.3, Natural Gas Processing). The average gross heating value of natural gas is approximately 1020 British thermal units per standard cubic foot (Btu/scf), usually varying from 950 to 1050 Btu/scf.

### 1.4.2 Firing Practices<sup>3-5</sup>

There are three major types of boilers used for natural gas combustion in the industrial, commercial, and utility sectors: watertube, firetube, and cast iron. Natural gas is also used in residential furnaces. Watertube boilers are designed to pass water through the inside of heat transfer tubes while the outside of the tubes is heated by direct contact with the hot combustion gases. The watertube design is the most common mechanism used for heat transfer in utility and large industrial boilers. Watertube boilers are used for a variety of applications, ranging from the provision of large amounts of process steam, to providing hot water or steam for space heating, to the generation of high-temperature, high-pressure steam for electricity production.

In firetube boilers, the hot combustion gases flow through the tubes, and the water being heated circulates outside of the tubes. These boilers are used primarily for heating systems, industrial process steam, and portable power boilers. Firetube boilers are almost exclusively packaged units. The two major types of firetube units are firebox boilers and Scotch Marine boilers.

In cast iron boilers, as in firetube boilers, the hot gases are contained inside the tubes and the water being heated circulates outside the tubes. However, the units are constructed of cast iron rather than steel. Virtually all cast iron boilers are constructed as package boilers. These boilers are used to produce either low-pressure steam or hot water, and are most commonly used in small commercial applications.

In residential furnaces, natural gas and air are combined in a burner and mixed to promote efficient combustion. Combustion air is supplied by a small fan in forced air furnaces. Hot combustion gases exchange heat with circulating air before being exhausted from a vent or chimney. A variety of burner types may be used in residential furnaces, including single port, multiport, inshot, ribbon, and slotted. Heat exchangers are typically of the sectional or drum types. Materials of construction for burners and heat exchangers include cast iron, stamped steel, and tube steel.

### 1.4.3 Emissions<sup>3-4</sup>

Natural gas is considered to be one of the cleanest of the commonly used fossil fuels. The emissions from natural gas-fired boilers and furnaces include nitrogen oxides ( $NO_x$ ), carbon monoxide ( $CO_1$ ), and carbon dioxide ( $CO_2$ ), and trace amounts of sulfur dioxide ( $SO_2$ ), particulate matter (PM), organic compounds, and other greenhouse gases.

### Nitrogen Oxides -

Nitrogen oxides are the major pollutants of concern when burning natural gas.  $NO_x$  formed in combustion processes are due either to thermal fixation of atmospheric nitrogen in the combustion air, resulting in the formation of thermal  $NO_x$ , or to the conversion of chemically bound nitrogen in the fuel, resulting in fuel  $NO_x$ . Due to its characteristically low fuel nitrogen content, nearly all  $NO_x$  emissions from natural gas combustion are thermal  $NO_x$ . The formation of thermal  $NO_x$  is affected by four furnace-zone factors: (1) nitrogen concentration, (2) oxygen concentration, (3) peak temperature, and (4) time of exposure at peak temperature. The emission trends due to changes in these factors are fairly consistent for all types of natural gas-fired boilers and furnaces. Emission levels vary considerably with the type and size of combustor and with operating conditions (particularly combustion air temperature, load, and excess air level in boilers).

#### Carbon Monoxide -

The rate of CO emissions from boilers depends on the efficiency of natural gas combustion. In some cases, the addition of  $NO_x$  control systems such as low  $NO_x$  burners and flue gas recirculation (FGR) will reduce combustion efficiency, resulting in higher CO (and trace organics) emissions relative to uncontrolled boilers.

### Sulfur Oxides -

Emissions of  $SO_2$  from natural gas-fired boilers are low because natural gas typically contains less than 0.1 percent sulfur. Sulfur-containing mercaptan, however, is added to natural gas for detection purposes, leading to small amounts of  $SO_2$  emissions.

#### Particulate Matter -

Because natural gas is a gaseous fuel, filterable particulate matter emissions are typically low. Particulate matter (PM) from natural gas combustion has been estimated to be less than 1 micrometer in size. Particulate matter is composed of filterable and condensable fractions, based on the EPA Method 5. Filterable and condensable emission rates are of the same order of magnitude for boilers; for residential furnaces, most of the PM is in the form of condensable material.

### Organics -

The rate of trace organic emissions from boilers and furnaces also depends on combustion efficiency. Organic emissions are minimized by combustion practices that promote high combustion temperatures, long residence times at those temperatures, and turbulent mixing of fuel and combustion air. Trace amounts of organic species in the natural gas fuel (e. g., ethylene and benzene) may also contribute to organic species emissions if they are not completely combusted in the boiler.

### Greenhouse Gases -6-11

Carbon dioxide ( $CO_2$ ), methane ( $CH_4$ ), and nitrous oxide ( $N_2O$ ) emissions are all produced during natural gas combustion. In properly tuned boilers, nearly all of the fuel carbon (99 percent) in natural gas is converted to  $CO_2$  during the combustion process. This conversion is relatively independent of firing configuration. Although the formation of CO acts to reduce  $CO_2$  emissions, the amount of CO produced is insignificant compared to the amount of  $CO_2$  produced. The majority of the fuel carbon not converted to  $CO_2$  is due to incomplete combustion.

Formation of  $N_2O$  during the combustion process is governed by a complex series of reactions and its formation is dependent upon many factors. Formation of  $N_2O$  is minimized when combustion temperatures are kept high (above 1475°F) and excess air is kept to a minimum (less than 1 percent).

Methane emissions are highest during periods of low-temperature combustion or incomplete combustion, such as the start-up or shut-down cycle for boilers. Typically, conditions that favor formation of  $N_2O$  also favor emissions of  $CH_4$ .

1.4.4 Controls<sup>4,12</sup>

NO, Controls -

Currently, the two most prevalent combustion  $NO_x$  control techniques being applied to natural gas-fired boilers (which result in characteristic changes in emission rates) are low  $NO_x$  burners and flue gas recirculation. Low  $NO_x$  burners reduce  $NO_x$  by accomplishing the combustion process in stages. Staging partially delays the combustion process, resulting in a cooler flame which suppresses  $NO_x$  formation. The two most common types of low  $NO_x$  burners being applied to natural gas-fired boilers are staged air burners and staged fuel burners.  $NO_x$  emission reductions of 40 to 85 percent (relative to uncontrolled emission levels) have been observed with low  $NO_x$  burners. Other combustion staging techniques which have been applied to natural gas-fired boilers include low excess air, reduced air preheat, and staged combustion (e. g., burners-out-of-service and overfire air). The degree of staging is a key operating parameter influencing  $NO_x$  emission rates for these systems.

In a flue gas recirculation (FGR) system, a portion of the flue gas is recycled from the stack to the burner windbox. Upon entering the windbox, the gas is mixed with combustion air prior to being fed to the burner. The FGR system reduces NO<sub>x</sub> emissions by two mechanisms. The recycled flue gas comprises combustion products which act as inerts during combustion of the fuel/air mixture. This additional mass is heated in the combustion zone, thereby lowering the peak flame temperature and reducing the amount of NO<sub>x</sub> formed. To a lesser extent, FGR also reduces NO<sub>x</sub> formation by lowering the oxygen concentration in the primary flame zone. The amount of flue gas recirculated is a key operating parameter influencing NO<sub>x</sub> emission rates for these systems. Flue gas recirculation is normally used in combination with specially designed low NO<sub>x</sub> burners capable of improved flame holding. When used in combination, these techniques are capable of reducing uncontrolled NO<sub>x</sub> emissions by 60 to 90 percent.

Two postcombustion technologies that may be applied to natural gas-fired boilers to reduce  $NO_x$  emissions by further amounts are selective noncatalytic reduction (SNCR) and selective catalytic reduction (SCR). The SNCR system involves injecting ammonia (or urea) into combustion flue gases (in a specific temperature zone) to reduce  $NO_x$  emission. The SCR system involves injecting  $NH_3$  in the presence of a catalyst to reduce  $NO_x$  emissions.

Emission factors for natural gas combustion in boilers and furnaces are presented in Tables 1.4-1, 1.4-2, 1.4-3, 1.4-4, and 1.4-5. Tables in this section present emission factors on a volume basis (lb/10<sup>6</sup>ft<sup>3</sup>). To convert to an energy basis (lb/MMBtu), divide by a heating value of 1000 MMBtu/10<sup>6</sup>ft<sup>3</sup>. For the purposes of developing emission factors, natural gas combustors have been organized into four general categories: utility/large industrial boilers, small industrial boilers, commercial boilers, and residential furnaces. Boilers and furnaces within these categories share the same general design and operating characteristics and hence have similar emission characteristics when combusting natural gas. The primary factor used to demarcate the individual combustor categories is heat input.

#### 1.4.5 Updates Since the Fifth Edition

The Fifth Edition was released in January 1995. Revisions to this section since that date are summarized below. For further detail, consult the memoranda describing each supplement or the

background report for this section. These and other documents can be found on the CHIEF electronic bulletin board (919-541-5742), or on the new EFIG home page (http://www.epa.gov/oar/oaqps/efig/).

### Supplement A, February 1996

The CO emission factor was changed from 27 to 15 lb/10<sup>6</sup> ft<sup>3</sup>.

### Supplement B, October 1996

- Text was added concerning firing practices.
- Text was added concerning emissions of NO<sub>x</sub>, SO<sub>x</sub>, CO, CO<sub>2</sub>, and organics.
- Text was added concerning controls from utility boilers.
- CO emission factors were updated for commercial LNB and NO<sub>x</sub> for large and small industrial and utility boilers.
- The condensable PM emission factors was updated for small industrial and commercial boilers, and the filterable PM emission factor was updated for residential boilers. A CO<sub>2</sub> emission factor was added for utility boilers.
- In the table with NO<sub>x</sub> emission factors, the Low NO<sub>x</sub> burner factor for utility/large industrial boilers changed from 81 to 79 lb/10<sup>6</sup> BTU, and the footnote for the uncontrolled factor was corrected.
- Figure 1.4-1, the load reduction coefficient as a function of boiler load, was removed.
- N<sub>2</sub>O emission factors were added.
- New factors were added for toxic organic and toxic metals emissions.

-	SC	O <sub>2</sub> <sup>b</sup>	NO	c x	C	$O^d$	N <sub>2</sub>	O°
Combustor Type (Size, 10 <sup>6</sup> Btu/hr Heat Input) (SCC)	Emission Factor (lb/10 <sup>6</sup> ft <sup>3</sup> )	EMISSION FACTOR RATING						
Utility/large Industrial Boilers (>100) (1-01-006-01, 1-01-006-04)								
Uncontrolled	0.6	Α	550 <sup>f</sup>	Α	40	<b>A</b>	2.2	С
Controlled - Low NO <sub>x</sub> burners	0.6	Α	79	D	ND	NA	0.64	E
Controlled - Flue gas recirculation	0.6	Α	53	D	ND	NA	NA	NA
Small Industrial Boilers (10 - 100) (1-02-006-02)								
Uncontrolled	0.6	Α	140	Α	35	Α	2.2 <sup>g</sup>	E
Controlled - Low NO, burners	0.6	· <b>A</b>	83	Ď	61	D	0.64 <sup>g</sup>	E
Controlled - Flue gas recirculation	0.6	Α	30	С	34	С	NA	NA
Commercial Boilers (0.3 - <10) (1-03-006-03)								
Uncontrolled	0.6	Α	100	В	21	С	2.2 <sup>g</sup>	<b>E</b> 、
Controlled - Low NO <sub>x</sub> burners	0.6	Α	17	С	· 15	С	0.64 <sup>g</sup>	E
Controlled - Flue gas recirculation	0.6	Α	36	D	ND	NA	NA	NA
Residential Furnaces (<0.3) (No SCC)								
Uncontrolled	0.6	Α	94	В	40	В	NA	NA

<sup>&</sup>lt;sup>a</sup> Units are lb of pollutant/10<sup>6</sup> cubic feet natural gas fired. To convert from lb/10<sup>6</sup> ft<sup>3</sup> to kg/10<sup>6</sup> m<sup>3</sup>, multiply by 16.0. Based on an average natural gas fired higher heating value of 1000 Btu/scf. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. SCC = Source Classification Code. ND = no data. NA = not applicable.

b References 13-14. Based on average sulfur content of natural gas, 2000 gr/10<sup>6</sup> scf. c References 12-13,15-19. Expressed as NO<sub>2</sub>.
d References 5,12-13,17-18,20-21.

e References 6-7.

f For tangentially fired units, use 275 lb/10<sup>6</sup> ft<sup>3</sup>. Note: This number was originally developed for AP-42 based on limited data. No additional data are available to refine this number.

g No data; based on the factors for utility boilers.

Table 1.4-2. EMISSION FACTORS FOR PARTICULATE MATTER (PM)
FROM NATURAL GAS COMBUSTION<sup>a</sup>

	Filteral	ole PM <sup>b</sup>	Condensable PM <sup>c</sup>		
Combustor Type (Size, 10 <sup>6</sup> Btu/hr Heat Input) (SCC)	Emission Factor (lb/10 <sup>6</sup> ft <sup>3</sup> )	EMISSION FACTOR RATING	Emission Factor (lb/10 <sup>6</sup> ft <sup>3</sup> )	EMISSION FACTOR RATING	
Utility/large industrial boilers (>100) (1-01-006-01, 1-01-006-04)	1 - 5	В	ND	NA	
Small industrial boilers (10 - 100) (1-02-006-02)	6.2	В	7.8	D	
Commercial boilers (0.3 - <10) (1-03-006-03)	4.5	С	7.4	С	
Residential furnaces (<0.3) (No SCC)	0.17	С	11	D	

a References 5,15,22-25. All factors represent uncontrolled emissions. Units are 1b of pollutant/10<sup>6</sup> cubic feet natural gas fired. To convert from 1b/10<sup>6</sup> ft<sup>3</sup> to kg/10<sup>6</sup> m<sup>3</sup>, multiply by 16.0. Based on an average natural gas higher heating value of 1000 Btu/scf. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. SCC = Source Classification Code. ND = no data. NA = not applicable.

<sup>&</sup>lt;sup>b</sup> Filterable PM is that particulate matter collected on or prior to the filter of an EPA Method 5 (or equivalent) sampling train.

<sup>&</sup>lt;sup>c</sup> Condensable PM is that particulate matter collected using EPA Method 202 (or equivalent). Total PM is the sum of the filterable PM and condensable PM. All PM emissions can be assumed to be less than 10 micrometers in aerodynamic equivalent diameter (PM-10).

Table 1.4-3. EMISSION FACTORS FOR CARBON DIOXIDE (CO2) AND TOTAL ORGANIC COMPOUNDS (TOC) FROM NATURAL GAS COMBUSTION<sup>a</sup>

	co	) <sub>2</sub> <sup>b</sup>	TOC°		
Combustor Type (Size, 10 <sup>6</sup> Btu/hr Heat Input) (SCC)	Emission Factor (lb/10 <sup>6</sup> ft <sup>3</sup> )	EMISSION FACTOR RATING	Emission Factor (lb/10 <sup>6</sup> ft <sup>3</sup> )	EMISSION FACTOR RATING	
Utility/large industrial boilers (>100) (1-01-006-01, 1-01-006-04)	1.2 E+05	В	1.7 <sup>d</sup>	С	
Small industrial boilers (10 - 100) (1-02-006-02)	1.2 E+05	В	5.8 <sup>e</sup>	C	
Commercial boilers (0.3 - <10) (1-03-006-03)	1.2 E+05	В	5.8	С	
Residential furnaces (No SCC)	1.2 E+05	В	11	D	

<sup>&</sup>lt;sup>a</sup> All factors represent uncontrolled emissions. Units are lb of pollutant/10<sup>6</sup> cubic feet. To convert from lb/10<sup>6</sup> ft<sup>3</sup> to kg/10<sup>6</sup> m<sup>3</sup>, multiply by 16.0. Based on an average natural gas higher heating value of 1000 Btu/scf. The emission factors in this table may be converted to other natural gas heating values by multiplying the given factor by the ratio of the specified heating value to this average heating value. SCC = Source Classification Code. ND = no data. NA = not applicable.

b References 8,15,27-29. c References 5,13,15,30.

d Reference 30: methane comprises 17% of organic compounds.
e Reference 30: methane comprises 52% of organic compounds.

Table 1.4-4. EMISSION FACTORS FOR SPECIATED ORGANIC COMPOUNDS FROM NATURAL GAS COMBUSTION<sup>2</sup>

Organic Compound	Average Emission Factor (lb/million ft <sup>3</sup> )	Emission Factor Rating
Formaldehyde	1.55E-01 <sup>b</sup>	С
Toluene	2.20E-03 <sup>c</sup>	E
2-Methylnaphthalene	9.02E-06 <sup>c</sup>	E
Naphthalene	2.40E-04 <sup>c</sup>	E
Fluoranthene	3.01E-06 <sup>c</sup>	E
Phenanthrene	1.00E-05 <sup>c</sup>	E
Pyrene	5.01E-06 <sup>c</sup>	E

<sup>&</sup>lt;sup>a</sup> Data are based on boilers that were both controlled and uncontrolled for criteria pollutant emissions. Source Classification Codes 1-01-006-01, 1-01-006-04. To convert from lb/million ft<sup>3</sup> to kg/million m<sup>3</sup>, multiply by 16.0.

Table 1.4-5. EMISSION FACTORS FOR METALS FROM NATURAL GAS COMBUSTION<sup>a</sup>

EMISSION FACTOR RATING: E

Metal	Average Emission Factor <sup>b</sup> (lb/million ft <sup>3</sup> )
Arsenic	2.30E-04
Barium	2.40E-03
Chromium	1.10E-03
Cobalt	1.20E-04
Copper	2.51E-04
Lead	2.71E-04
Manganese	3.81E-04
Molybdenum	5.81E-04
Nickel	3.61E-03
Vanadium	3.21E-03

<sup>&</sup>lt;sup>a</sup> Data are for natural gas boilers controlled with overfire air and flue gas recirculation. Source Classification Codes 1-01-006-04.

b References 31-36.

c Reference 32. Based on data from one source test.

b Reference 32. Based on data from one source test. To convert from lb/million ft<sup>3</sup> to kg/million m<sup>3</sup>, multiply by 16.0.

#### 1.3 Fuel Oil Combustion

### 1.3.1 General 1-3

Two major categories of fuel oil are burned by combustion sources: distillate oils and residual oils. These oils are further distinguished by grade numbers, with Nos. 1 and 2 being distillate oils; Nos. 5 and 6 being residual oils; and No. 4 being either distillate oil or a mixture of distillate and residual oils. No. 6 fuel oil is sometimes referred to as Bunker C. Distillate oils are more volatile and less viscous than residual oils. They have negligible nitrogen and ash contents and usually contain less than 0.3 percent sulfur (by weight). Distillate oils are used mainly in domestic and small commercial applications, and include kerosene and diesel fuels. Being more viscous and less volatile than distillate oils, the heavier residual oils (Nos. 5 and 6) may need to be heated for ease of handling and to facilitate proper atomization. Because residual oils are produced from the residue remaining after the lighter fractions (gasoline, kerosene, and distillate oils) have been removed from the crude oil, they contain significant quantities of ash, nitrogen, and sulfur. Residual oils are used mainly in utility, industrial, and large commercial applications.

### 1.3.2 Firing Practices<sup>4</sup>

The major boiler configurations for fuel oil-fired combustors are watertube, firetube, cast iron, and tubeless design. Boilers are classified according to design and orientation of heat transfer surfaces, burner configuration, and size. These factors can all strongly influence emissions as well as the potential for controlling emissions.

Watertube boilers are used in a variety of applications ranging from supplying large amounts of process steam to providing space heat for industrial facilities. In a watertube boiler, combustion heat is transferred to water flowing through tubes which line the furnace walls and boiler passes. The tube surfaces in the furnace (which houses the burner flame) absorb heat primarily by radiation from the flames. The tube surfaces in the boiler passes (adjacent to the primary furnace) absorb heat primarily by convective heat transfer.

Firetube boilers are used primarily for heating systems, industrial process steam generators, and portable power boilers. In firetube boilers, the hot combustion gases flow through the tubes while the water being heated circulates outside of the tubes. At high pressures and when subjected to large variations in steam demand, firetube units are more susceptible to structural failure than watertube boilers. This is because the high-pressure steam in firetube units is contained by the boiler walls rather than by multiple small-diameter watertubes, which are inherently stronger. As a consequence, firetube boilers are typically small and are used primarily where boiler loads are relatively constant. Nearly all firetube boilers are sold as packaged units because of their relatively small size.

A cast iron boiler is one in which combustion gases rise through a vertical heat exchanger and out through an exhaust duct. Water in the heat exchanger tubes is heated as it moves upward through the tubes. Cast iron boilers produce low pressure steam or hot water, and generally burn oil or natural gas. They are used primarily in the residential and commercial sectors.

Another type of heat transfer configuration used on smaller boilers is the tubeless design. This design incorporates nested pressure vessels with water in between the shells. Combustion gases are fired into the inner pressure vessel and are then sometimes recirculated outside the second vessel.

### 1.3.3 Emissions<sup>5</sup>

Emissions from fuel oil combustion depend on the grade and composition of the fuel, the type and size of the boiler, the firing and loading practices used, and the level of equipment maintenance. Because the combustion characteristics of distillate and residual oils are different, their combustion can produce significantly different emissions. In general, the baseline emissions of criteria and noncriteria pollutants are those from uncontrolled combustion sources. Uncontrolled sources are those without add-on air pollution control (APC) equipment or other combustion modifications designed for emission control. Baseline emissions for sulfur dioxide (SO<sub>2</sub>) and particulate matter (PM) can also be obtained from measurements taken upstream of APC equipment.

### 1.3.3.1 Particulate Matter Emissions<sup>6-15</sup> -

Particulate matter emissions depend predominantly on the grade of fuel fired. Combustion of lighter distillate oils results in significantly lower PM formation than does combustion of heavier residual oils. Among residual oils, firing of No. 4 or No. 5 oil usually produces less PM than does the firing of heavier No. 6 oil.

In general, PM emissions depend on the completeness of combustion as well as on the oil ash content. The PM emitted by distillate oil-fired boilers primarily comprises carbonaceous particles resulting from incomplete combustion of oil and is not correlated to the ash or sulfur content of the oil. However, PM emissions from residual oil burning are related to the oil sulfur content. This is because low-sulfur No. 6 oil, either refined from naturally low-sulfur crude oil or desulfurized by one of several processes, exhibits substantially lower viscosity and reduced asphaltene, ash, and sulfur contents, which results in better atomization and more complete combustion.

Boiler load can also affect particulate emissions in units firing No. 6 oil. At low load (50 percent of maximum rating) conditions, particulate emissions from utility boilers may be lowered by 30 to 40 percent and by as much as 60 percent from small industrial and commercial units. However, no significant particulate emission reductions have been noted at low loads from boilers firing any of the lighter grades. At very low load conditions (approximately 30 percent of maximum rating), proper combustion conditions may be difficult to maintain and particulate emissions may increase significantly.

### 1.3.3.2 Sulfur Oxides Emissions 1-2,6-9,16 -

Sulfur oxides  $(SO_x)$  emissions are generated during oil combustion from the oxidation of sulfur contained in the fuel. The emissions of  $SO_x$  from conventional combustion systems are predominantly in the form of  $SO_2$ . Uncontrolled  $SO_x$  emissions are almost entirely dependent on the sulfur content of the fuel and are not affected by boiler size, burner design, or grade of fuel being fired. On average, more than 95 percent of the fuel sulfur is converted to  $SO_2$ , about 1 to 5 percent is further oxidized to sulfur trioxide  $(SO_3)$ , and 1 to 3 percent is emitted as sulfate particulate.  $SO_3$  readily reacts with water vapor (both in the atmosphere and in flue gases) to form a sulfuric acid mist.

### 1.3.3.3 Nitrogen Oxides Emissions 1-2,6-10,15,17-27 -

Oxides of nitrogen  $(NO_x)$  formed in combustion processes are due either to thermal fixation of atmospheric nitrogen in the combustion air ("thermal  $NO_x$ "), or to the conversion of chemically bound nitrogen in the fuel ("fuel  $NO_x$ "). The term  $NO_x$  refers to the composite of nitric oxide (NO) and nitrogen dioxide (NO<sub>2</sub>). Test data have shown that for most external fossil fuel combustion systems, over 95 percent of the emitted  $NO_x$  is in the form of nitric oxide (NO). Nitrous oxide (N<sub>2</sub>O) is not included in  $NO_x$  but has recently received increased interest because of atmospheric effects.

Experimental measurements of thermal  $NO_x$  formation have shown that  $NO_x$  concentration is exponentially dependent on temperature, and proportional to  $N_2$  concentration in the flame, the square root of  $O_2$  concentration in the flame, and the residence time. Thus, the formation of thermal  $NO_x$  is affected by four factors: (1) peak temperature, (2) fuel nitrogen concentration, (3) oxygen concentration, and (4) time of exposure at peak temperature. The emission trends due to changes in these factors are generally consistent for all types of boilers: an increase in flame temperature, oxygen availability, and/or residence time at high temperatures leads to an increase in  $NO_x$  production.

Fuel nitrogen conversion is the more important  $NO_x$ -forming mechanism in residual oil boilers. It can account for 50 percent of the total  $NO_x$  emissions from residual oil firing. The percent conversion of fuel nitrogen to  $NO_x$  varies greatly, however; typically from 20 to 90 percent of nitrogen in oil is converted to  $NO_x$ . Except in certain large units having unusually high peak flame temperatures, or in units firing a low nitrogen content residual oil, fuel  $NO_x$  generally accounts for over 50 percent of the total  $NO_x$  generated. Thermal fixation, on the other hand, is the dominant  $NO_x$ -forming mechanism in units firing distillate oils, primarily because of the negligible nitrogen content in these lighter oils. Because distillate oil-fired boilers are usually smaller and have lower heat release rates, the quantity of thermal  $NO_x$  formed in them is less than that of larger units which typically burn residual oil.<sup>28</sup>

A number of variables influence how much  $NO_x$  is formed by these two mechanisms. One important variable is firing configuration.  $NO_x$  emissions from tangentially (corner) fired boilers are, on the average, less than those of horizontally opposed units. Also important are the firing practices employed during boiler operation. Low excess air (LEA) firing, flue gas recirculation (FGR), staged combustion (SC), reduced air preheat (RAP), low  $NO_x$  burners (LNBs), or some combination thereof may result in  $NO_x$  reductions of 5 to 60 percent. Load reduction (LR) can likewise decrease  $NO_x$  production. Nitrogen oxide emissions may be reduced from 0.5 to 1 percent for each percentage reduction in load from full load operation. It should be noted that most of these variables, with the exception of excess air, only influence the  $NO_x$  emissions of large oil-fired boilers. Low excess air-firing is possible in many small boilers, but the resulting  $NO_x$  reductions are less significant.

### 1.3.3.4 Carbon Monoxide Emissions<sup>29-32</sup> -

The rate of carbon monoxide (CO) emissions from combustion sources depends on the oxidation efficiency of the fuel. By controlling the combustion process carefully, CO emissions can be minimized. Thus if a unit is operated improperly or not well maintained, the resulting concentrations of CO (as well as organic compounds) may increase by several orders of magnitude. Smaller boilers, heaters, and furnaces tend to emit more of these pollutants than larger combustors. This is because smaller units usually have a higher ratio of heat transfer surface area to flame volume than larger combustors have; this leads to reduced flame temperature and combustion intensity and, therefore, lower combustion efficiency.

The presence of CO in the exhaust gases of combustion systems results principally from incomplete fuel combustion. Several conditions can lead to incomplete combustion, including insufficient oxygen (O<sub>2</sub>) availability; poor fuel/air mixing; cold-wall flame quenching; reduced combustion temperature; decreased combustion gas residence time; and load reduction (i. e., reduced combustion intensity). Since various combustion modifications for NO<sub>x</sub> reduction can produce one or more of the above conditions, the possibility of increased CO emissions is a concern for environmental, energy efficiency, and operational reasons.

### 1.3.3.5 Organic Compound Emissions<sup>29-39</sup> -

Small amounts of organic compounds are emitted from combustion. As with CO emissions, the rate at which organic compounds are emitted depends, to some extent, on the combustion

efficiency of the boiler. Therefore, any combustion modification which reduces the combustion efficiency will most likely increase the concentrations of organic compounds in the flue gases.

Total organic compounds (TOCs) include VOCs, semi-volatile organic compounds, and condensable organic compounds. Emissions of VOCs are primarily characterized by the criteria pollutant class of unburned vapor phase hydrocarbons. Unburned hydrocarbon emissions can include essentially all vapor phase organic compounds emitted from a combustion source. These are primarily emissions of aliphatic, oxygenated, and low molecular weight aromatic compounds which exist in the vapor phase at flue gas temperatures. These emissions include all alkanes, alkenes, aldehydes, carboxylic acids, and substituted benzenes (e. g., benzene, toluene, xylene, and ethyl benzene).

The remaining organic emissions are composed largely of compounds emitted from combustion sources in a condensed phase. These compounds can almost exclusively be classed into a group known as polycyclic organic matter (POM), and a subset of compounds called polynuclear aromatic hydrocarbons (PAH or PNA). There are also PAH-nitrogen analogs. Information available in the literature on POM compounds generally pertains to these PAH groups.

Formaldehyde is formed and emitted during combustion of hydrocarbon-based fuels including coal and oil. Formaldehyde is present in the vapor phase of the flue gas. Formaldehyde is subject to oxidation and decomposition at the high temperatures encountered during combustion. Thus, larger units with efficient combustion (resulting from closely regulated air-fuel ratios, uniformly high combustion chamber temperatures, and relatively long gas retention times) have lower formaldehyde emission rates than do smaller, less efficient combustion units.

### 1.3.3.6 Trace Element Emissions<sup>29-32,40-44</sup> -

Trace elements are also emitted from the combustion of oil. For this update of AP-42, trace metals included in the list of 189 hazardous air pollutants under Title III of the 1990 Clean Air Act Amendments are considered. The quantity of trace elements entering the combustion device depends solely on the fuel composition. The quantity of trace metals emitted from the source depends on combustion temperature, fuel feed mechanism, and the composition of the fuel. The temperature determines the degree of volatilization of specific compounds contained in the fuel. The fuel feed mechanism affects the separation of emissions into bottom ash and fly ash. In general, the quantity of any given metal emitted depends on the physical and chemical properties of the element itself; concentration of the metal in the fuel; the combustion conditions; and the type of particulate control device used, and its collection efficiency as a function of particle size.

Some trace metals concentrate in certain waste particle streams from a combustor (bottom ash, collector ash, flue gas particulate), while others do not. Various classification schemes to describe this partitioning have been developed. The classification scheme used by Baig, et al.<sup>44</sup> is as follows:

- Class 1: Elements which are approximately equally distributed between fly ash and bottom ash, or show little or no small particle enrichment.
- Class 2: Elements which are enriched in fly ash relative to bottom ash, or show increasing enrichment with decreasing particle size.
- Class 3: Elements which are emitted in the gas phase.

By understanding trace metal partitioning and concentration in fine particulate, it is possible to postulate the effects of combustion controls on incremental trace metal emissions. For example, several NO<sub>x</sub> controls for boilers reduce peak flame temperatures (e. g., SC, FGR, RAP, and LR). If combustion temperatures are reduced, fewer Class 2 metals will initially volatilize, and fewer will be available for subsequent condensation and enrichment on fine PM. Therefore, for combustors with particulate controls, lower volatile metal emissions should result due to improved particulate removal. Flue gas emissions of Class 1 metals (the non-segregating trace metals) should remain relatively unchanged.

Lower local  $O_2$  concentrations is also expected to affect segregating metal emissions from boilers with particle controls. Lower  $O_2$  availability decreases the possibility of volatile metal oxidation to less volatile oxides. Under these conditions, Class 2 metals should remain in the vapor phase as they enter the cooler sections of the boiler. More redistribution to small particles should occur and emissions should increase. Again, Class 1 metal emissions should remain unchanged.

### 1.3.3.7 Greenhouse Gases<sup>45-50</sup> -

Carbon dioxide ( $CO_2$ ), methane ( $CH_4$ ), and nitrous oxide ( $N_2O$ ) emissions are all produced during fuel oil combustion. Nearly all of the fuel carbon (99 percent) in fuel oil is converted to  $CO_2$  during the combustion process. This conversion is relatively independent of firing configuration. Although the formation of CO acts to reduce  $CO_2$  emissions, the amount of CO produced is insignificant compared to the amount of  $CO_2$  produced. The majority of the fuel carbon not converted to  $CO_2$  is due to incomplete combustion in the fuel stream.

Formation of  $N_2O$  during the combustion process is governed by a complex series of reactions and its formation is dependent upon many factors. Formation of  $N_2O$  is minimized when combustion temperatures are kept high (above  $1475^{\circ}F$ ) and excess air is kept to a minimum (less than 1 percent). Additional sampling and research is needed to fully characterize  $N_2O$  emissions and to understand the  $N_2O$  formation mechanism. Emissions can vary widely from unit to unit, or even from the same unit at different operating conditions. Average emission factors based on reported test data have been developed for conventional oil combustion systems.

Methane emissions vary with the type of fuel and firing configuration, but are highest during periods of incomplete combustion or low-temperature combustion, such as the start-up or shut-down cycle for oil-fired boilers. Typically, conditions that favor formation of  $N_2O$  also favor emissions of  $CH_4$ .

#### 1.3.4 Controls

Control techniques for criteria pollutants from fuel oil combustion may be classified into three broad categories: fuel substitution, combustion modification, and postcombustion control. Emissions of noncriteria pollutants such as particulate phase metals have been controlled through the use of post combustion controls designed for criteria pollutants. Fuel substitution reduces  $SO_2$  or  $NO_x$  and involves burning a fuel with a lower sulfur or nitrogen content, respectively. Particulate matter will generally be reduced when a lighter grade of fuel oil is burned.<sup>6,8,11</sup> Combustion modification includes any physical or operational change in the furnace or boiler and is applied primarily for  $NO_x$  control purposes, although for small units, some reduction in PM emissions may be available through improved combustion practice. Postcombustion control is a device after the combustion of the fuel and is applied to control emissions of PM,  $SO_2$ , and  $NO_x$ .

### 1.3.4.1 Particulate Matter Controls<sup>51</sup> -

Control of PM emissions from residential and commercial units is accomplished by improving burner servicing and by incorporating appropriate equipment design changes to improve oil atomization and combustion aerodynamics. Optimization of combustion aerodynamics using a flame retention device, swirl, and/or recirculation is considered to be the best approach toward achieving the triple goals of low PM emissions, low NO<sub>x</sub> emissions, and high thermal efficiency.

Large industrial and utility boilers are generally well-designed and well-maintained so that soot and condensable organic compound emissions are minimized. Particulate matter emissions are more a result of emitted fly ash with a carbon component in such units. Therefore, postcombustion controls (mechanical collectors, ESP, fabric filters, etc.) are necessary to reduce PM emissions from these sources where local regulations dictate.

Mechanical collectors, a prevalent type of control device, are primarily useful in controlling particulates generated during soot blowing, during upset conditions, or when a very dirty heavy oil is fired. For these situations, high-efficiency cyclonic collectors can achieve up to 85 percent control of particulate. Under normal firing conditions, or when a clean oil is combusted, cyclonic collectors are not nearly so effective because of the high percentage of small particles (less than 3 micrometers in diameter) emitted.

Electrostatic precipitators (ESPs) are commonly used in oil-fired power plants. Older precipitators, usually small, typically remove 40 to 60 percent of the emitted PM. Because of the low ash content of the oil, greater collection efficiency may not be required. Currently, new or rebuilt ESPs can achieve collection efficiencies of up to 90 percent.

In fabric filtration, a number of filtering elements (bags) along with a bag cleaning system are contained in a main shell structure incorporating dust hoppers. The particulate removal efficiency of the fabric filter system is dependent on a variety of particle and operational characteristics including particle size distribution, particle cohesion characteristics, and particle electrical resistivity. Operational parameters that affect collection efficiency include air-to-cloth ratio, operating pressure loss, cleaning sequence, interval between cleaning, and cleaning intensity. The structure of the fabric filter, filter composition, and bag properties also affect collection efficiency. Collection efficiencies of baghouses may be more than 99 percent.

Scrubbing systems have also been installed on oil-fired boilers to control both sulfur oxides and particulate. These systems can achieve SO<sub>2</sub> removal efficiencies of 90 to 95 percent and particulate control efficiencies of 50 to 60 percent.

### 1.3.4.2 SO<sub>2</sub> Controls<sup>52-53</sup> -

Commercialized postcombustion flue gas desulfurization (FGD) processes use an alkaline reagent to absorb SO<sub>2</sub> in the flue gas and produce a sodium or a calcium sulfate compound. These solid sulfate compounds are then removed in downstream equipment. Flue gas desulfurization technologies are categorized as wet, semi-dry, or dry depending on the state of the reagent as it leaves the absorber vessel. These processes are either regenerable (such that the reagent material can be treated and reused) or nonregenerable (in which case all waste streams are de-watered and discarded).

Wet regenerable FGD processes are attractive because they have the potential for better than 95 percent sulfur removal efficiency, have minimal waste water discharges, and produce a saleable sulfur product. Some of the current nonregenerable calcium-based processes can, however, produce a saleable gypsum product.

To date, wet systems are the most commonly applied. Wet systems generally use alkali slurries as the SO<sub>x</sub> absorbent medium and can be designed to remove greater than 90 percent of the incoming SO<sub>x</sub>. Lime/limestone scrubbers, sodium scrubbers, and dual alkali scrubbing are among the commercially proven wet FGD systems. Effectiveness of these devices depends not only on control device design but also on operating variables.

### 1.3.4.3 NO<sub>x</sub> Controls<sup>41,54-55</sup> -

In boilers fired on crude oil or residual oil, the control of fuel  $NO_x$  is very important in achieving the desired degree of  $NO_x$  reduction since fuel  $NO_x$  typically accounts for 60 to 80 percent of the total  $NO_x$  formed. Fuel nitrogen conversion to  $NO_x$  is highly dependent on the fuel-to-air ratio in the combustion zone and, in contrast to thermal  $NO_x$  formation, is relatively insensitive to small changes in combustion zone temperature. In general, increased mixing of fuel and air increases nitrogen conversion which, in turn, increases fuel  $NO_x$ . Thus, to reduce fuel  $NO_x$  formation, the most common combustion modification technique is to suppress combustion air levels below the theoretical amount required for complete combustion. The lack of oxygen creates reducing conditions that, given sufficient time at high temperatures, cause volatile fuel nitrogen to convert to  $N_2$  rather than NO.

Several techniques are used to reduce  $NO_x$  emissions from fuel oil combustion. In addition to fuel substitution, the primary techniques can be classified into one of two fundamentally different methods — combustion controls and postcombustion controls. Combustion controls reduce  $NO_x$  by suppressing  $NO_x$  formation during the combustion process while postcombustion controls reduce  $NO_x$  emissions after their formation. Combustion controls are the most widely used method of controlling  $NO_x$  formation in all types of boilers and include low excess air, burners out of service, biased-burner firing, flue gas recirculation, overfire air, and low- $NO_x$  burners. Postcombustion control methods include selective noncatalytic reduction (SNCR) and selective catalytic reduction (SCR). These controls can be used separately, or combined to achieve greater  $NO_x$  reduction.

Operating at low excess air involves reducing the amount of combustion air to the lowest possible level while maintaining efficient and environmentally compliant boiler operation. NO<sub>x</sub> formation is inhibited because less oxygen is available in the combustion zone. Burners out of service involves withholding fuel flow to all or part of the top row of burners so that only air is allowed to pass through. This method simulates air staging, or overfire air conditions, and limits NO<sub>x</sub> formation by lowering the oxygen level in the burner area. Biased-burner firing involves firing the lower rows of burners more fuel-rich than the upper row of burners. This method provides a form of air staging and limits NO<sub>x</sub> formation by limiting the amount of oxygen in the firing zone. These methods may change the normal operation of the boiler and the effectiveness is boiler-specific. Implementation of these techniques may also reduce operational flexibility; however, they may reduce NO<sub>x</sub> by 10 to 20 percent from uncontrolled levels.

Flue gas recirculation involves extracting a portion of the flue gas from the economizer section or air heater outlet and readmitting it to the furnace through the furnace hopper, the burner windbox, or both. This method reduces the concentration of oxygen in the combustion zone and may reduce NO<sub>x</sub> by as much as 40 to 50 percent in some boilers.

Overfire air is a technique in which a percentage of the total combustion air is diverted from the burners and injected through ports above the top burner level. Overfire air limits  $NO_x$  by (1) suppressing thermal  $NO_x$  by partially delaying and extending the combustion process resulting in less intense combustion and cooler flame temperatures; (2) a reduced flame temperature that limits thermal  $NO_x$  formation, and/or (3) a reduced residence time at peak temperature which also limits thermal  $NO_x$  formation.

Low  $NO_x$  burners are applicable to tangential and wall-fired boilers of various sizes. They have been used as a retrofit  $NO_x$  control for existing boilers and can achieve approximately 35 to 55 percent reduction from uncontrolled levels. They are also used in new boilers to meet NSPS limits. Low  $NO_x$  burners can be combined with overfire air to achieve even greater  $NO_x$  reduction (40 to 60 percent reduction from uncontrolled levels).

SNCR is a postcombustion technique that involves injecting ammonia or urea into specific temperature zones in the upper furnace or convective pass. The ammonia or urea reacts with  $NO_x$  in the flue gas to produce nitrogen and water. The effectiveness of SNCR depends on the temperature where reagents are injected; mixing of the reagent in the flue gas; residence time of the reagent within the required temperature window; ratio of reagent to  $NO_x$ ; and the sulfur content of the fuel that may create sulfur compound that deposit in downstream equipment. There is not as much commercial experience to base effectiveness on a wide range of boiler types; however, in limited applications,  $NO_x$  reductions of 25 to 40 percent have been achieved.

SCR is another postcombustion technique that involves injecting ammonia into the flue gas in the presence of a catalyst to reduce  $NO_x$  to nitrogen and water. The SCR reactor can be located at various positions in the process including before an air heater and particulate control device, or downstream of the air heater, particulate control device, and flue gas desulfurization systems. The performance of SCR is influenced by flue gas temperature, fuel sulfur content, ammonia to  $NO_x$  ratio, inlet  $NO_x$  concentration, space velocity, and catalyst condition.  $NO_x$  emission reductions of 75 to 85 percent have been achieved through the use of SCR on oil-fired boilers operating in the U.S.

Tables 1.3-1 and 1.3-2 present emission factors for uncontrolled criteria pollutants from fuel oil combustion. Tables in this section present emission factors on a volume basis (lb/10<sup>3</sup>gal). To convert to an energy basis (lb/MMBtu), divide by a heating value of 150 MMBtu/10<sup>3</sup>gal for Nos. 4, 5, 6, and residual fuel oil, and 140 MMBtu/10<sup>3</sup>gal for No. 2 and distillate fuel oil. Tables 1.3-3, 1.3-4, 1.3-5, and 1.3-6 present cumulative size distribution data and size-specific emission factors for particulate emissions from uncontrolled and controlled fuel oil combustion. Figures 1.3-1, 1.3-2, 1.3-3, and 1.3-4 present size-specific emission factors for particulate emissions from uncontrolled and controlled fuel oil combustion. Emission factors for N<sub>2</sub>O, POM, and formaldehyde are presented in Table 1.3-7. Emission factors for speciated organic compounds are presented in Table 1.3-8. Emission factors for trace elements are given in Table 1.3-9. Emission factors for metals are given in Table 1.3-10. Default emission factors for CO<sub>2</sub> are presented in Table 1.3-11. A summary of various SO<sub>2</sub> and NO<sub>x</sub> controls for fuel-oil-fired boilers is presented in Table 1.3-12 and 1.3-13, respectively.

### 1.3.5 Updates Since the Fifth Edition

The Fifth Edition was released in January 1995. Revisions to this section since that date are summarized below. For further detail, consult the memoranda describing each supplement or the background report for this section. These and other documents can be found on the CHIEF electronic bulletin board (919-541-5742), or on the new EFIG home page (http://www.epa.gov/oar/oaqps/efig/).

### Supplement A, February 1996

The formulas presented in the footnotes for filterable PM were moved into the table.

For  $SO_2$  and  $SO_3$  emission factors, text was added to the table footnotes to clarify that "S" is a weight percent and not a fraction. A similar clarification was made to the CO and  $NO_x$  footnotes. SCC A2104004/A2104011 was provided for residential furnaces.

For industrial boilers firing No. 6 and No. 5 oil, the methane emission factor was changed from 1 to 1.0 to show two significant figures.

For SO<sub>2</sub> and SO<sub>3</sub> factors, text was added to the table footnotes to clarify that "S" is a weight percent and not a fraction.

- The N<sub>2</sub>O, POM, and formaldehyde factors were corrected.
- Table 1.3-10 was incorrectly labeled 1.1-10. This was corrected.

### Supplement B, October 1996

Text was added concerning firing practices.

Factors for  $N_2O$ , POM, and formaldehyde were added.

New data for filterable PM were used to create a new PM factor for residential oil-fired furnaces.

Many new factors were added for toxic organics, toxic metals from distillate oil, and toxic metals from residual oil.

A table was added for new CO<sub>2</sub> emission factors.

Table 1.3-1. CRITERIA POLLUTANT EMISSION FACTORS FOR UNCONTROLLED FUEL OIL COMBUSTION<sup>a</sup>

	sc	) <sub>2</sub> b	SC	)3 <sup>c</sup>	NO	O <sub>x</sub> d	CC	Oe't	Filterabl	e PM <sup>g</sup>
Firing Configuration (SCC) <sup>2</sup>	Emission Factor (lb/10 <sup>3</sup> gal)	EMISSION FACTOR RATING								
Utility boilers									_	
No. 6 oil fired, normal firing (1-01-004-01)	157S	A	5.7S	С	67	Α	5	Α	9.19(S)+3.22	A
No. 6 oil fired, tangential firing (1-01-004-04)	157S	A	5.7\$	С	42	A	5	A	9.19(S)+3.22	Α
No. 5 oil fired, normal firing (1-01-004-05)	157S	A	5.75	С	67	Α	5	<b>A</b>	10	В
No. 5 oil fired, tangential firing (1-01-004-06)	157S	A	5.7\$	С	42	A	5	Α	10	В
No. 4 oil fired, normal firing (1-01-005-04)	150S	A	5.7S	С	67	A	5	· <b>A</b>	7	В
No. 4 oil fired, tangential firing (1-01-005-05)	150S	A	5.7S	С	42	A	5	A	7	В
Industrial										
No. 6 oil fired (1-02-004-01/02/03)	157S	Α	2S	Α	55	Α	5	A	9.19(S)+3.22	Α
No. 5 oil fired (1-02-004-04)	157S	Α	28	Α	55	Α	5	Α	10	В
Distillate oil fired (1-02-005-01/02/03)	142\$	A	2\$	A	20	Α	5	Α	2	Α
No. 4 oil fired (1-02-005-04)	150S	Α	2S	Α	20	Α	5	Α	7	В
Commercia Vinstitutional										
No. 6 oil fired (1-03-004-01/02/03)	157S	Α	28	. <b>A</b>	55	. <b>A</b>	5	Α	9.19(S)+3.22	Α
No. 5 oil fired (1-03-004-04)	157S	Α	28	Α	55	Α	5	Α	10	В
Distillate oil fired (1-03-005-01/02/03)	142S	A	28	Α	20	A	5	Α	2	A
No. 4 oil fired (1-03-005-04)	150S	Α	28	Α	20	Α	5	Α	7	В
Residential furnace (A2104004/A2104011)	1428	A	2S	A	18	A	5	A	0.4 <sup>h</sup>	В

### Table 1.3-1 (cont.).

<sup>a</sup> To convert from  $1b/10^3$  gal to kg/ $10^3$  L, multiply by 0.120. SCC = Source Classification Code.

b References 1-2,6-9,14,56-60. S indicates that the weight % of sulfur in the oil should be multiplied by the value given. For example, if the fuel is 1% sulfur, then S = 1.

c References 1-2,6-8,16,57-60. S indicates that the weight % of sulfur in the oil should be multiplied by the value given. For example, if

the fuel is 1% sulfur, then S = 1.

d References 6-7,15,19,22,56-62. Expressed as NO<sub>2</sub>. Test results indicate that at least 95% by weight of NO<sub>x</sub> is NO for all boiler types except residential furnaces, where about 75% is NO. For utility vertical fired boilers use 105 lb/10<sup>3</sup> gal at full load and normal (>15%) excess air. Nitrogen oxides emissions from residual oil combustion in industrial and commercial boilers are related to fuel nitrogen content, estimated by the following empirical relationship: lb NO<sub>2</sub> /10<sup>3</sup> gal = 20.54 + 104.39(N), where N is the weight % of nitrogen in the oil. For example, if the fuel is 1% nitrogen, then N = 1.

e References 6-8,14,17-19,56-61. CO emissions may increase by factors of 10 to 100 if the unit is improperly operated or not well

maintained.

f Emission factors for CO<sub>2</sub> from oil combustion should be calculated using 1b CO<sub>2</sub>/10<sup>3</sup> gal oil = 256C (Distillate), 286C (Residual), or 250C (Kerosene) where C indicates weight % of carbon in the oil. For example, if the fuel is 86% carbon, then C = 86.

References 6-8,10,13-15,56-60,62-63. Filterable PM is that particulate collected on or prior to the filter of an EPA Method 5 (or equivalent) sampling train. Particulate emission factors for residual oil combustion are, on average, a function of fuel oil sulfur content where S is the weight % of sulfur in oil. For example, if fuel oil is 1% sulfur, then S = 1.

h Based on data from new burner designs. Pre-1970's burner designs may emit filterable PM as high as 3.0 1b/10<sup>3</sup> gal.

# Table 1.3-2. EMISSION FACTORS FOR TOTAL ORGANIC COMPOUNDS (TOC), METHANE, AND NONMETHANE TOC (NMTOC) FROM UNCONTROLLED FUEL OIL COMBUSTION<sup>a</sup>

### EMISSION FACTOR RATING: A

Firing Configuration (SCC)	TOC <sup>b</sup> Emission Factor (lb/10 <sup>3</sup> gal)	Methane <sup>b</sup> Emission Factor (lb/10 <sup>3</sup> gal)	NMTOC <sup>b</sup> Emission Factor (lb/10 <sup>3</sup> gal)
Utility boilers			
No. 6 oil fired, normal firing (1-01-004-01)	1.04	0.28	0.76
No. 6 oil fired, tangential firing (1-01-004-04)	1.04	0.28	0.76
No. 5 oil fired, normal firing (1-01-004-05)	1.04	0.28	0.76
No. 5 oil fired, tangential firing (1-01-004-06)	1.04	0.28	0.76
No. 4 oil fired, normal firing (1-01-005-04)	1.04	0.28	0.76
No. 4 oil fired, tangential firing (1-01-005-05)	1.04	0.28	0.76
Industrial boilers			
No. 6 oil fired (1-02-004-01/02/03)	1.28	1.00	0.28
No. 5 oil fired (1-02-004-04)	1.28	1.00	0.28
Distillate oil fired (1-02-005-01/02/03)	0.252	0.052	0.2
No. 4 oil fired (1-02-005-04)	0.252	0.052	0.2
Commercial/institutional/residential combustors			
No. 6 oil fired (1-03-004-01/02/03)	1.605	0.475	1.13
No. 5 oil fired (1-03-004-04)	1.605	0.475	1.13
Distillate oil fired (1-03-005-01/02/03)	0.556	0.216	0.34
No. 4 oil fired (1-03-005-04)	0.556	0.216	0.34
Residential furnace (A2104004/A2104011)	2.493	1.78	0.713

<sup>&</sup>lt;sup>a</sup> To convert from lb/10<sup>3</sup> gal to kg/10<sup>3</sup> L, multiply by 0.12. SCC = Source Classification Code. b References 29-32. Volatile organic compound emissions can increase by several orders of magnitude if the boiler is improperly operated or is not well maintained.

Table 1.3-3. CUMULATIVE PARTICLE SIZE DISTRIBUTION AND SIZE-SPECIFIC EMISSION FACTORS FOR UTILITY BOILERS FIRING RESIDUAL OIL<sup>a</sup>

		lative M Stated S		Cumulative Emission Factor (lb/10 <sup>3</sup> gal)					
		Co	ntrolled	Uncont	trolled <sup>c</sup>	ESP Contr	olled <sup>d</sup>	Scrubber C	Controlled <sup>e</sup>
Particle Size <sup>b</sup> (µm)	Uncon- trolled	ESP	Scrubber	Emission Factor	EMISSION FACTOR RATING	Emission Factor	EMISSION FACTOR RATING	Emission Factor	EMISSION FACTOR RATING
15	80	75	100	6.7A	. с	0.05A	Е	0.50A	D
10	- 71	63	100	5.9A	С	0.042A	E	0,50A <del>0.05</del> 0A	D
6	58	52	100	4.8A	С	0.035A	<b>E</b>	0.50A	D
2.5	52	41	97	4.3A	С	0.028A	E	0.48A	D
1.25	43	31	91	3.6A	С	0.021A	E	0.46A	D
1.00	39	28	84	3.3A	C	0.018A	E	0.42A	D
0.625	20	20	64	1.74	С	0.007A	E	0.32A	D
TOTAL	100	100	100	8.3A	С	0.067A	E	0.50A	D

a Reference 26. Source Classification Codes 1-01-004-01/04/05/06 and 1-01-005-04/05. To convert from lb/10<sup>3</sup> gal to kg/m<sup>3</sup>, multiply by 0.120. ESP = electrostatic precipitator.

No. 6 oil: 
$$A = 939(S) = 320 lb/10^3 gal$$
  
No. 5 oil:  $A = 10 lb/10^3 gal$ 

b Expressed as aerodynamic equivalent diameter.

<sup>&</sup>lt;sup>c</sup> Particulate emission factors for residual oil combustion without emission controls are, on average, a function of fuel oil grade and sulfur content where S is the weight % of sulfur in the oil. For example, if the fuel is 1.00% sulfur, then S = 1.

No. 4 oil: A = 7 lb/10<sup>3</sup> gal

d Estimated control efficiency for ESP is 99.2%.

e Estimated control efficiency for scrubber is 94%

Table 1.3-4. CUMULATIVE PARTICLE SIZE DISTRIBUTION AND SIZE-SPECIFIC EMISSION FACTORS FOR INDUSTRIAL BOILERS FIRING RESIDUAL OIL<sup>a</sup>

	Cumulative Ma	ss % ≤ Stated Size	Factor <sup>c</sup> (lb/10 <sup>3</sup> gal)	tor <sup>c</sup> (lb/10 <sup>3</sup> gal)		
			Uncontrol	led	Multiple Cyclone	Controlled <sup>d</sup>
Particle Size <sup>b</sup> (μm)	Uncontrolled	Multiple Cyclone Controlled	Emission Factor	EMISSION FACTOR RATING	Emission Factor	EMISSION FACTOR RATING
15	91	100	7.59A	D	1.67A	E
10	86	95	7.17A	D	1.58A	E
6	77	72	6.42A	D .	1.17A	E
2.5	56	22	4.67A	D	0.33A	E
1.25	39	21	3.25A	D	0.33A	E
1.00	36	21	3.00A	D	0.33A	E
0.625	30	e	2.50A	D	e	NA
TOTAL	100	100	8.34A	D	1.67A	E

a Reference 26. Source Classification Codes 1-02-004-01/02/03/04 and 1-02-005-04. To convert from lb/10<sup>3</sup> gal to kg/10<sup>3</sup> L, multiply by 0.120. NA = not applicable.

b Expressed as aerodynamic equivalent diameter.

No. 6 oil: 
$$A = 9.19(S) + 3.22 \text{ lb/}10^3 \text{ gal}$$

<sup>&</sup>lt;sup>c</sup> Particulate emission factors for residual oil combustion without emission controls are, on average, a function of fuel oil grade and sulfur content where S is the weight % of sulfur in the oil. For example, if the fuel is 1.0% sulfur, then S = 1.

No. 6 oil: A = 9.19(S) + 3.22 lb/10<sup>3</sup> gal

No. 5 oil: A = 10 lb/10<sup>3</sup> gal

No. 4 oil: A = 7 lb/10<sup>3</sup> gal

d Estimated control efficiency for multiple cyclone is 80%.

e Insufficient data.

### Table 1.3-5. CUMULATIVE PARTICLE SIZE DISTRIBUTION AND SIZE-SPECIFIC EMISSION FACTORS FOR UNCONTROLLED INDUSTRIAL BOILERS FIRING DISTILLATE OILa

#### EMISSION FACTOR RATING: E

Particle Size <sup>b</sup> (μm)	Cumulative Mass % ≤ Stated Size	Cumulative Emission Factor (lb/10 <sup>3</sup> gal)
15	68	1.33
10	50	1.00
6	30	0.58
2.5	12	0.25
1.25	9	0.17
1.00	8	0.17
0.625	2	0.04
TOTAL	100	2.00

<sup>&</sup>lt;sup>a</sup> Reference 26. Source Classification Codes 1-02-005-01/02/03. To convert from lb/10<sup>3</sup> gal to  $kg/10^3$  L, multiply by 0.12.

Table 1.3-6. CUMULATIVE PARTICLE SIZE DISTRIBUTION AND SIZE-SPECIFIC EMISSION FACTORS FOR UNCONTROLLED COMMERCIAL BOILERS BURNING RESIDUAL OR DISTILLATE OIL<sup>a</sup>

#### EMISSION FACTOR RATING: D

	Cumulative Mass % ≤ Stated Size			nission Factor <sup>c</sup> ) <sup>3</sup> gal)
Particle Size <sup>b</sup> (μm)	Residual Oil	Distillate Oil	Residual Oil	Distillate Oil
15	78	60	6.50A	1.17
10	62	55	5.17A	1.08
6	44	49	3.67A	1.00
2.5	23	42	1.92A	0.83
1.25	16	. 38	1.33A	0.75
1.00	14	37	1.17A	0.75
0.625	13	35	1.08A	0.67
TOTAL	100	100	8.34A	2.00

Reference 26. Source Classification Codes: 1-03-004-01/02/03/04 and 1-03-005-01/02/03/04. To convert from lb/10<sup>3</sup> gal to kg/10<sup>3</sup> L, multiply by 0.12.
 Expressed as aerodynamic equivalent diameter.
 Particulate emission factors for residual oil combustion without emission controls are, on average, a

b Expressed as aerodynamic equivalent diameter.

function of fuel oil grade and sulfur content where S is the weight % of sulfur in the fuel. For example, if the fuel is 1.0% sulfur, then S = 1.

No. 6 oil:  $A = 9.19(S) + 3.22 \text{ lb/}10^3 \text{ gal.}$ No. 5 oil:  $A = 10 \text{ lb/}10^3 \text{ gal.}$ No. 4 oil:  $A = 7 \text{ lb/}10^3 \text{ gal.}$ No. 2 oil:  $A = 2 \text{ lb/}10^3 \text{ gal.}$ 

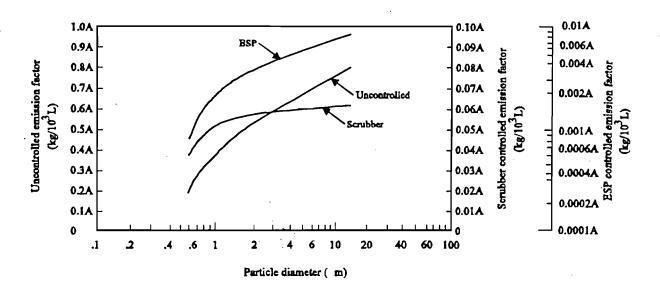


Figure 1.3-1. Cumulative size-specific emission factors for utility boilers firing residual oil.

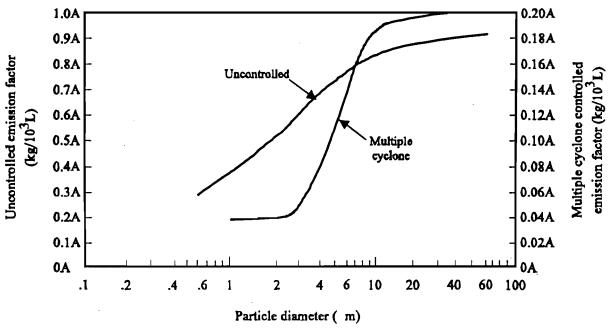


Figure 1.3-2. Cumulative size-specific emission factors for industrial boilers firing residual oil.

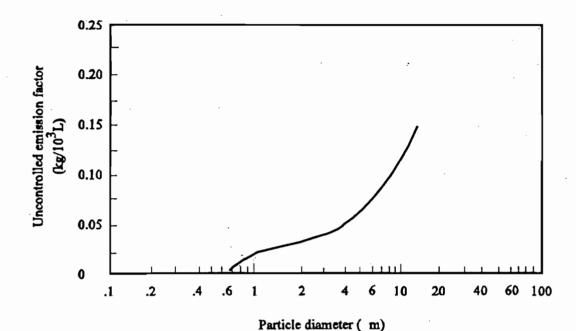


Figure 1.3-3. Cumulative size-specific emission factors for uncontrolled industrial boilers firing distillate oil.

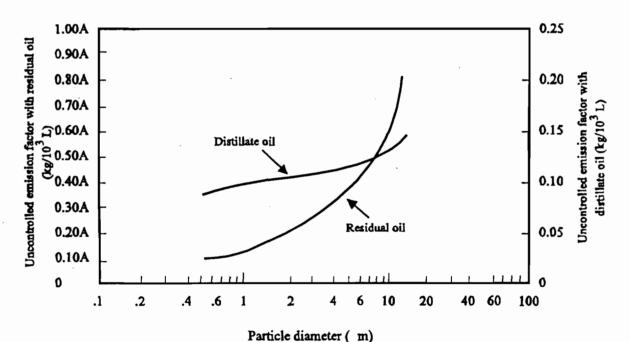


Figure 1.3-4. Cumulative size-specific emission factors for uncontrolled commercial boilers burning residual and distillate oil.

### Table 1.3-7. EMISSION FACTORS FOR NITROUS OXIDE (N2O), POLYCYCLIC ORGANIC MATTER (POM), AND FORMALDEHYDE (HCOH) FROM FUEL OIL COMBUSTION<sup>a</sup>

### EMISSION FACTOR RATING: E

Firing Configuration	Emission Factor (lb/10 <sup>3</sup> gal)				
(SCC)	N <sub>2</sub> O <sup>b</sup>	POM <sup>c</sup>	HCOH <sup>c</sup>		
Utility/industrial/commercial boilers					
No. 6 oil fired (1-01-004-01, 1-02-004-01, 1-03-004-01)	0.11	0.0011 - 0.0013 <sup>d</sup>	0.024 - 0.061		
Distillate oil fired (1-01-005-01, 1-02-005-01, 1-03-005-01)	0.11	0.0033 <sup>e</sup>	0.035 - 0.061		
Residential furnaces (A2104004/A2104011)	0.05	ND	ND		

<sup>&</sup>lt;sup>a</sup> To convert from  $1b/10^3$  gal to  $kg/10^3$ L, multiply by 0.12. SCC = Source Classification Code. ND = no data.

ND = no data.

b References 45-46. EMISSION FACTOR RATING = B.
c References 29-32.
d Particulate and gaseous POM.
e Particulate POM only.

Table 1.3-8. EMISSION FACTORS FOR SPECIATED ORGANIC COMPOUNDS FROM FUEL OIL COMBUSTION<sup>a</sup>

	Average Emission	EMISSION
	Factor <sup>b</sup>	FACTOR
Organic Compound	(lb/10 <sup>3</sup> Gal)	RATING
Benzene	2.14E-04	<b>C</b> .
Ethylbenzene	6.36E-05 <sup>c</sup>	E
Formaldehyde <sup>d</sup>	3.30E-02	C
Naphthalene	1.13E-03	C
1,1,1-Trichloroethane	2.36E-04 <sup>c</sup>	E
Toluene	6.20E-03	D
o-Xylene	1.09E-04 <sup>c</sup>	E
Acenaphthene	2.11E-05	C
Acenaphthylene	2.53E-07	D
Anthracene	1.22E-06	C
Benz(a)anthracene	4.01E-06	С
Benzo(b,k)fluoranthene	1.48E-06	C
Benzo(g,h,i)perylene	2.26E-06	C
Chrysene	2.38E-06	· C
Dibenzo(a,h) anthracene	1.67E-06	D D
Fluoranthene	4.84E-06	C
Fluorene	4.47E-06	C
Indo(1,2,3-cd)pyrene	2.14E-06	C
Phenanthrene	1.05E-05	C
Pyrene	4.25E-06	С
OCDD	3.10E-09 <sup>c</sup>	E

<sup>&</sup>lt;sup>a</sup> Data are for residual oil fired boilers, Source Classification Codes (SCCs) 1-01-004-01/04.

<sup>b</sup> References 64-72. To convert from lb/10<sup>3</sup> gal to kg/10<sup>3</sup> L, multiply by 0.12.

<sup>c</sup> Based on data from one source test (Reference 67).

<sup>&</sup>lt;sup>d</sup> The formaldehyde number presented here is based only on data from utilities using No. 6 oil. The number presented in Table 1.3-7 is based on utility, commercial, and industrial boilers.

## Table 1.3-9. EMISSION FACTORS FOR TRACE ELEMENTS FROM DISTILLATE FUEL OIL COMBUSTION SOURCES<sup>a</sup>

### EMISSION FACTOR RATING: E

Firing Configuration	Emission Factor (lb/10 <sup>12</sup> Btu)										
(SCC)	As	Ве	Cd	Со	Cr	Hg	Mn	Ni	Pb	Sb	Se
Distillate oil fired (1-01-005-01, 1-02-005-01, 1-03-005-01)	4.2	2.5	11	ND	48-67	3.0	14	170	8.9	ND	ND

a References 29-32,40-44. The emission factors in this table represent the ranges of factors reported in the literature. If only one data point was found, it is still reported in this table. To convert from lb/10<sup>12</sup> Btu to pg/J, multiply by 0.43. SCC = Source Classification Code. ND = no data.

Table C-1. Summary of BACT Determinations for NOx from Boilers Fired by Natural Gas

Company	State	Permit No.	Permit Issue Date	Throughput	Emssion Limit	Control Equipment	Control Efficience
BUCKNELL UNIVERSITY	PA	60-0001A	11/26/97	24000 lb/hr Steam	0.1 lb/MMBlu		
GRAIN PROCESSING CORP.	IN	CP 027-7239-00046	06/10/97	244 MMBtu/hr	0.05 lb/MMBtu	LOW NOX BURNERS AND FLUE GAS RECIRCULATION (FGR)	
KERN MEDICAL CENTER	CA	S-1678-11-0	01/27/97	3 MMBtu/hr		OPERATION LIMITED TO 80% UTILIZATION. RECORD/EEPING REQUIRED FOR COMPLIANCE	_
CALIFORNIA STATE PRISON, CORCORAN	CA	C-0214-32-0	01/15/97	8.1 MMBtu/hr	0.012 MMBlu/hr	PREMIXED LEAN BURN COMBUSTION TECHNOLOGY	_
DARLING INTERNATIONAL	ÇA	C-406-3-1	12/30/96	31.2 MMBtu/hr	0.036 lb/MMBlu	LOW-NOX BURNER, FLUE GAS RECIRCULATION (FGR)	_
IMC-AGRICO COMPANY - FAUSTINA PLANT	LA	PSD-LA-602	10/16/96	320 MMBlu/hr	0.08 lb/MMBtu	LOW NOX BURNERS	_
O.H. KRUSE GRAIN AND MILLING	CA	S-160-13-0	09/19/96	10 MMBtu/hr	0.106 lb/MMBtu	<del>-</del>	
WEYERHAEUSER COMPANY	MS	1680-44	09/10/96	7 MMBtu/hr	80 PPMVD @ 8% O2	STAGED COMBUSTION	
WEYERHAEUSER COMPANY	MS	1680-44	09/10/96	1600 MMBtu/hr	0.5 lb/MMBtu	CONTINUED EFFICIENT OPERATION WITH LOW NOX BURNERS	-
WEYERHAEUSER COMPANY	MS	1680-44	09/10/96	400 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNERS WITH FLUE GAS RECIRCULATION (FGR)	-
TOYOTA MOTOR CORPORATION SVCS OF N.A.	IN	CP-051-5391-00037	08/09/96	58 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNERS & FUEL SPEC: USE OF NATURAL GAS 111 AS FUEL	-
BOISE CASCADE CORP.	AL	102-1	05/10/96	346.4 MMBtu/hr	0.05 lb/MMB(u	LOW NOX BURNERS AND FLUE GAS RECIRCULATION (FGR)	
MID-GEORGIA COGEN.	GA	4911-76-11753	04/03/96	60 MMBtu/hr	0.1 lb/MMBlu	DRY LOW NOX BURNER WITH FGR	_
EXXON COMPANY, USA SANTA YNEZ UNIT PROJECT	CA	ATC-9517	02/05/96	95 MMBtu/hr - each	27 PPMVD AT 3% O2	FLUE-GAS RECIRCULATION (FGR). STEAM INJECTION	-
SITIX OF PHOENIX, INC.	AZ	950460	02/01/96	42 MMBtu/hr	49 TPY	FLUE GAS RECIRCULATION (FGR)-NOX NOT TO EXCEED 30 PPM	-
MINNESOTA CORN PROCESSORS	MN MS	8300038-19	08/09/95	770 1410: -	24.1 lb/hr	USE OF LOW NOX MULTISTAGE COMBUSTION COMBINED WITHINDUCED FLUE GAS RECIRCULATION (FGR)	-
GEORGIA PACIFIC CORP. (MONTICELLO MILL) TRANSAMERICAN REFINING CORPORATION	LA	1500-7 PSD-LA-571 (M-1)	07/11/95	776 MMBtu/hr	40.0 % %	NO PHYSICAL MODIFICATION TO BOILER. BACT NOT REQUIRED.	-
KAMINE/BESICORP SYRACUSE LP	NY	313201 2010/00001-00007	02/10/95 12/10/94	244 MMBtu/hr	19.8 lb/hr	LOW NOX BURNERS/COMBUSTION CONTROL	-
KAMINE/BESICORP SYRACUSE LP	NY	313201 2010/00001-00007	12/10/94	2.5 MMBtu/hr 33 MMBtu/hr	0.12 lb/MMBtu	INDUCED FLUE CAS DECIDENTATION (FCD)	70.0
COURTAULDS FIBERS, INC.	AL	503-5002-X023 AND -X24	11/02/94	148 MMBtu/hr	0.035 lb/MMBtu 10.4 lb/hr	INDUCED FLUE GAS RECIRCULATION (FGR) LOW NOX BURNERS WITH 8% FLUE GAS RECIRCULATION	70.9 87
JVC MAGNETICS AMERICA CO.	AL	413-0040-X001,X002,X003,X006	06/16/94	5.2 MMBlu/hr	40 TPY	FUEL SPEC: NATURAL GAS W/ MAX 0.5% SULFUR FUEL OILAS BACKUP	07
PORTLAND GENERAL ELECTRIC CO.	OR	25-31	05/31/94	361 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNER AND FLUE GAS RECIRCULATION	_
INTEL CORPORATION	AZ	93-46	04/10/94	50 MMBtu/hr	, 0.1 12/1/10/10	LOW NOX BURNERS	_
CHAMPION INTERNATIONAL CORP	FL	PSD-FL-200	03/25/94	533 MMBtu/hr	0.06 lb/MMBtu	COEN LOW NOX BURNERS AND FGR	_
STAFFORD RAILSTEEL CORPORATION	`AR	1471-A	08/17/93	46.5 MMBtu/hr	7.1 TPY	FUEL SPEC: USE OF NATURAL GAS & LOW NOX BURNERS	
LOCKPORT COGEN FACILITY	NY	292600 0446/00001-00007	07/14/93	210 MMBtu/hr	0.2 lb/MMBtu		
ANITEC COGEN PLANT	NY	030200 0451	07/07/93	123 MMBtu/hr	0.05 lb/MMBtu		_
NEWARK BAY COGENERATION PARTNERSHIP, L.P.	NJ	01-92-5231 TO 01-92-5261	06/09/93	206 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNERS, FLUE GAS RECIRCULATION (FGR)	_
NEWARK BAY COGENERATION PARTNERSHIP, L.P.	NJ	01-92-5231 TO 01-92-5261	06/09/93	200 MMBtuthr	0.05 lb/MMBtu	LOW NOX BURNERS, FLUE GAS RECIRCULATION (FGR)	_
INDECK ENERGY COMPANY	NY	563203 0099	05/12/93	0 MMBtu/hr	0.2 lb/MMBtu	-	
CNG TRANSMISSION CORPORATION	w	R13-1471/R14-9	05/03/93	10 MMBtu/hr	140 LB/MM cu ft	-	_
INDELK ENERGY SERVICES OF OTSEGO	MI	143-90	03/16/93	778 MMBtu/hr	0.25 lb/MMBtu	SNCR/DRY CONTROL	50
INDELK ENERGY SERVICES OF OTSEGO	M	143-90	03/16/93	99 MMBtu/hr	0.06 lb/MMBtu	FLUE GAS RECIRCULATION	40
TRANSAMERICAN REFINING CORPORATION (TARC)	LA	PSD-LA-571	01/15/93	1.2 MMBlu/hr	0.14 lb/hr	" · GOOD COMBUSTION PRACTICES	_
AMERICAN CRYSTAL SUGAR COMPANY	MN	29B-92-OT-1	12/15/92	200.1 MMBtu/hr	0.075 lb/MMBtu	LOW NOX BURNER WITH FLUE GAS RECIRCULATION BOILER INSTALLATION	-
KAMINE/BESICORP CORNING L.P.	NY	8-4638-22/1-0	11/05/92	33.5 MMBtu/hr	0.32 lb/MMBtu	LOW NOX BURNER, FGR	-
SUNLAND REFINERY	CA	S-0207-0085-00 & -0036-00	09/24/92	12.6 MMBtu/hr	0.036 lb/MMBtu	FGRAOW NOX BURNER	-
CPC - CORN PRODUCTS DIVISION	IL	91020069/ID 031012ABI	08/06/92	600 MMBtu/hr	0.05 lb/MMBtu	LOW NOX BURNER & FLUE GAS RECIRCULATION	85
SARANAC ENERGY COMPANY	NY	5-942-106/1-9	07/31/92	249 MMBtu/hr	0.136 lb/MMBtu	LOW NOX BURNERS	-
INDECK-YERKES ENERGY SERVICES	NY	146400 0133	06/24/92	99 MMBtu/hr	0.2 lb/MMBtu	<del>-</del>	
BOISE CASCADE CORPORATION	AL	102-1	04/01/92	343.4 MMBtwhr	0.05 lb/MMBtu	-	-
BERMUDA HUNDRED ENERGY LIMITED PARTNERSHIP KALAMAZOO POWER LIMITED	VA	51020	03/03/92	250 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNER	-
	MI	1234-90	12/03/91	500 KW	0.02 lb/MMBtu	-	
SCOTT PAPER COMPANY JAMES RIVER CORP	AL MI	503-2012	09/17/91	220.5 MMBtu/hr -	0.1 lb/MMBtu	FACILITY NOW SHUT DOWN.	_
MINNESOTA CORN PROCESSORS, INC.	MN	423-91 AMENDMENT 6 TO 1939-88-0T-1	09/17/91 06/25/91	226.7 MMBtu/hr	0.06 lb/MMBtu	LOW NOX BURNERS AND FGR SYS	70
CHAMPION INTERNATIONAL	AL	707-1-U54	05/08/91	178.7 MMBtu/hr 5.8 MMBtu/hr	0.125 lb/MMBtu 0.05 lb/MMBtu	LOW NOX BURNERS	-
NORTHERN CONSOLIDATED POWER	PA	25-328-1	05/03/91	100.4 MMBtwhr	0.1 lb/MMBtu	FLUE GAS RECIRCULATION	_
LAKEWOOD COGENERATION, L.P.	NJ	25-320-1	04/01/91		0.2 lb/MMBtu	LOWNOV BURNERS	50
LAKEWOOD COGENERATION, L.P.	NJ	-	04/01/91	131 MMBtu/hr 131 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNERS LOW NOX BURNERS	50
DEL MONTE FOODS, USA	CA	3040000000	09/26/90			BURNER JOHNSTON	30
I/N KOTE	IN	PC (71) 1822	11/20/89	20.9 MMBtu/hr 70,8 MMBtu/hr	40 PPMVD @ 3% O2	FUEL SPEC: USE OF NATURAL GAS & FLUE GAS RECIRC ULATION (FGR)	-
GENERAL ELECTRIC CO.	IN.	PSD (65) 1757	09/17/89	93 MMBtu/hr	0.05 lb/MMBtu 0.133 lb/MMBtu	STAGED COMBUSTION AIR & LOW EXCESS AIR	
GENERAL ELECTRIC CO.	iN	PSD (65) 1757	09/17/89	250 MMBtu/hr	0.12 lb/MMBtu	LOW NOX BURNERS, STAGED COMBUSTION AIR	_
		472800 2054		250 11111010111		2011107100-11211010000000000000000000000	

Source: EPA's RACT/BACT/LAER Clearinghouse, 1998

### APPENDIX D

NO<sub>x</sub> SOURCE INVENTORY

Table D-1. NO<sub>X</sub> Screening Analysis for the AAQS and PSD Class II Inventories for Stone Container Corporation (alphabetical listing)

			Relativ	e to Sto	ne Containe	er Facility	Screening Emission	Maximum Allowable	AAQS and/or PSD Class II
	UTM Coo	rdinates (km)	X	Υ	Distance	Direction	Threshold	Emissions	Modeling
Facility Name	E	N ,	(km)	(km)	(km)	(degrees)	(TPY)(a)		Analysis?
Amerada Hess Jacksonville	442.7	3365.0	0.7	-0.6	0.9	131	SIA	28.8	YES
Cedar Bay Cogeneration, Inc.	441.1	3365.1	-0.9	-0.5	1.1	240	-1	3,788	YES
Anheuser Busch, Inc Jacksonville	440.6	3366.8	-1.4	1.2	1.9	310	` 17	1,038	YES
Atlantic Coast Asphalt - Heckscher	440.0	3364.1	-2.0	-1.5	2.5	233	30	NA	NO
Stone Container Corp	439.2	3365.5	-2.8	-0.1	2.8	269	36	NA	NO
Quickrete-Jacksonville	439.8	3363.3	-2.2	-2.3	3.2	224	44	9	NO
J.B. Coxwell Contracting, Inc.	446.0	3365.9	4.0	0.3	4.0	85	59	47	NO
Interstate Brands Corporation	437.2	3366.3	-4.8	0.7	4.9	278	77	NA	NO
Jacksonville Electric Authority - SJRPP	446.9	3366.3	4.9	0.7	4.9	82	79	32,289	YES
City of Jacksonville - Solid Waste Division	446.5	3367.7	4.5	2.1	5.0	65	80	23	NO
U S Gypsum Co	438.9	3361.2	-3.1	-4.4	5.4	215	88	353	YES
Celotex Corp	446.4	3362.4	4.4	-3.2	5.5	126	90	76	NO
Jacksonville Electric Authority - Northside	447.7	3364.9	5.7	-0.7	5.7	97	95	15,286	YES
Support Terminal Operg. Part., L.P.	438.5	3360.5	-3.5	-5.1	6.2	214	104	9	NO
PCS Phosphate- Jacksonville	439.3	3359.8	-2.7	-5.8	6.4	205	108	27	NO
Jefferson Smurfit Corp (U.S.) - Jacksonville	439.9	3359.3	-2.1	-6.3	6.6	198	113	1,200	YES
Jacksonville Electric Authority - Kennedy	440.0	3359.2	-2.0	-6.4	6.7	. 197	114	4,245	YES
Millennium Specialty Chemicals	436.8	3360.7	-5.2	-4.9	7.1	227	122	189	YES
Coastal Fuels Marketing, Inc.	439.7	3358.7	-2.3	-6.9	7.3	198	125	16	NO
Jefferson Smurfit Corporation	440.0	3358.1	-2.0	-7.5	7.8	195	135	7	NO
BF Goodrich Co.Engineered Polymer Product		3365.5	8.0	-0.1	8.0	91	140	16	NO
Jacksonville Buckman Sewage Tretmnt Plnt	439.4	3357.7	-2.6	-7.9	8.3	198	146	NA	NO
Castleton Beverage Co	438.4	3373.9	-3.6	8.3	9.0	337	160	3	NO
Industrial Water Services, Inc.	439.5	3356.8	-2.5	-8.8	9.1	196	163	2	NO
Mulliniks Construction Co., Inc Portable Cr	433.7	3361.4	-8.4	-4.2	9.3	243	167	NA	NO
Turner Electric Works	438.2	3357.0	-3.8	-8.6	9.4	204	168	1	NO
Owens-Corning - Jacksonville	439.3	3356.0	-2.7	-9.6	10.0	196	179	15	NO
University Medical Center	436.5	3357.2	-5.5	-8.4	10.0	213	181	39	NO
Cookson Matthey Eagle	433.0	3358.5	-9.0	-7.1	11.5	232	209	NA	NO
Kraft Foods	437.5	3354.7	-4.5	-10.9	11.8	202	215	16	NO
Jacksonville Electric Authority - Southside	437.7	3353.9	-4.4	-11.8	12.5	200	231	1,349	YES
Gate Riverplace Co.	436.8	3354.2	-5.2	-11.4	12.6	204	231	74	NO
Pan Coatings Of Florida, Inc.	434.8	3355.1	-7.2	-10.5	12.7	214	234	NA	NO
Hardage Giddens Funeral Homes Of Jackson		3354.5	-7.2	-11.1	13.2	213	245	1	NO
Anchor Glass Container Corporation	431.3	3357.5	-10.7	-8.1	13.4	233	248	789	YES
Chemrock Corp	429.7	3359.6	-12.3	-6.0	13.7	244	254	2	NO

Table D-1. NO<sub>x</sub> Screening Analysis for the AAQS and PSD Class II Inventories for Stone Container Corporation (alphabetical listing)

			D. It'		0- 1-1		Screening	Maximum	AAQS and/o
	LITM Coo	rdinates (km)	X	ve to Sto	ne Containe Distance	r ⊢acility Direction	Emission Threshold	Allowable Emissions	PSD Class I Modeling
Facility Name	E	N	(km)	(km)	(km)	(degrees)	(TPY)(a)		Analysis?
Atlantic Dry Dock Corporation	455.8	3361.7	13.8	-3.9	14.3	106	267	7	NO
St Vincents Medical Center	434.6	3353.0	-7.4	-12.6	14.6	211	273	48	NO
Con Agra Feed Company	431.4	3355.3	-10.6	-10.3	14.8	226	276	NA	NO
Electro-Mechanical South, Inc.	427.0	3364.5	-15.0	-1.1	15.0	266	280	NA	NO
Baptist Medical Center	435.4	3352.0	-6.6	-13.6	15.1	206	282	773	YES
Wincup	428.2	3357.8	-13.8	-7.8	15.9	241	297	NA	NO
Metalplate Galvanizing	426.5	3362.0	-15.5	-3.6	15.9	257	298	NA	NO
General Electric Co	458.1	3364.5	16.1	-1.2	16.1	94	302	1	NO
Metal Container Corporation	428.4	3356.4	-13.6	-9.2	16.4	236	308	7	NO
Bush Boake Allen, Inc.	427.6	3357.3	-14.4	-8.3	16.6	240	312	96	NO
City Of Jacksonville(Girvin Rd Landfill)	455.4	3355.6	13.4	-10.0	16.7	127	315	· 77	NO
D-Graphics Div. Jefferson Smurfit Corp.	440.1	3348.4	-1.9	-17.2	17.3	186	326°	NA	NO
Reichhold Chemicals, Inc.	428.2	3355.0	-13.8	-10.7	17.4	232	329	14	NO
St Luke's Hospital Association	443.8	3346.9	1.8	-18.8	18.8	175	357	9	NO
U S Naval Station Mayport	460.4	3361.6	18.4	-4.0	18.8	102	357	56	NO
S & G Packaging L.L.C.	442.5	3386.1	0.5	20.5	20.5	1	390	2	NO
First Union Bank Of Florida	444.0	3342.8	2.0	-22.8	22.9	175	438	357	NO
E 3 Thermal Remediation Group - Nas Jax	434.2	3343.7	-7.8	-21.9	23.2	200	444	4	NO
United States Navy - Nas Jacksonville	434.2	3342.8	-7.8	-22.8	24.1	199	462	276	NO
Mayo Clinic Jacksonville	458.0	3347.5	16.0	-18.1	24.2	139	463	39	NO
Refuse Services, Inc.	442.3	3341.2	0.3	-24.4	24.5	179	469	14	NO
Ring Power Corp - Sunbeam Road	442.0	3341.0	0.0	-24.6	24.6	180	472	79	NO
David Coxwell	420.0	3353.7	-22.0	-11.9	25.0	242	481	23	NO
Duval Asphalt Products - Phillips Highway	441.8	3340.0	-0.2	-25.6	25.6	181	492	18	NO
Atlantic Coast Asphalt -, Shad	445.3	3339.7	3.3	-25.9	26.2	173	503	19	NO
Champion International Corp	416.5	3353.2	-25.5	-12.4	28.4	244	547	16	NO
Rayonier Inc.	454.7	3392.2	12.7	26.6	29.5	26	570	1,582	YES
J.B. Coxwell Contracting, Inc.	448.1	3336.6	6.1	-29.0	29.7	168	573	47	NO
Anderson Columbia, Inc #7	448.1	3336.5	6.1	-29.1	29.7	168	575	7	NO
Jefferson Smurfit Corp-Fernandina Beach	456.2	3394.2	14.2	28.6	31.9	26	619	5,058	YES
U S Naval Air Station - Cecil Field	415.2	3344.5	-26.8	-21.1	34.1	232	662	71	NO
Dawson Land Development, Co., Inc.	463.2	3335.6	21.2	-30.0	36.8	145	715	NA	NO
Dustcoating, Inc,	413.1	3342.9	-28.9	-22.7	36.8	232	715	8	NO
Ameristeel, Jacksonville,Mill Div.	405.9	3350.2	-36.1	-15.4	39.2	247	765	307	NO
Florida Solite Company	427.4	3326.5	-14.6	-39.1	41.7	200	815	108	NO
Tamko Roofing Products, Inc.	435.2	3316.8	-6.8	-48.8	49.3	188	965	NA	NO

Table D-1. NO<sub>x</sub> Screening Analysis for the AAQS and PSD Class II Inventories for Stone Container Corporation (alphabetical listing)

			Relativ	e to Sto	ne Containe	r Facility	Screening Emission	Maximum Allowable	AAQS and/or PSD Class II
	UTM Cool	rdinates (km)	Х	Υ	Distance	Direction	Threshold	Emissions	Modeling
Facility Name	E	N	(km)	(km)	(km)	(degrees)	(TPY)(a)	(TPY)	Analysis?
E.I. Dupont DE Nemours & CO- Highland	398.7	3325.0	-43.3	-40.6	59.4	227	1167	NA	NO

NA = Emissions not provided

- (a) Screening emissions threshold is 20 x [Distance (km) to facility -1 km], based on North Carolina Screening Method. A significant impact distance of 1 km was assumed for including competing NOx facilities into the inventory. Total screening area is 51 km from the SCC facility. All facilities emitting <1 TPY have been omitted.
- (b) Indicates PSD sources at this facility
  Stone Container Corporation Jacksonville facility UTM coordinates (km):
  442.0 3365.6
- (c) Sources within 1 km of the SCC site are modeled without regard to the screening criteria.

Source: Golder Associates, 1998

### APPENDIX E

 $\mathbf{NO}_{\mathbf{X}}$  SOURCES USED IN THE AAQS ANALYSIS

Table E-1. Summary of Individual Source Emission and Operating Parameters for the NO<sub>x</sub> AAQS Modeling Analysis

Facility ID		Facility Lo UTM E,N		APIS	Stack	Height	Stack D	iam.	Exit Veloc	eity	Tempe	rature	Allowable NO	x Emissions
Number	Facility Name	Relative X,	r' (m) ^a	Src #	(ft)	(m)	(ft)	(m)	(ft/s)	(m/s)	(°F)	(K)	lb/hr	TPY
0310001	Jacksonville Elect. Auth SJRPP	446.9 4900	3366.3 700	1 2	640 640	195.1 195.1	22.3 22.3	6.80 6.80	72.5 72.5	22.10 22.10	156 156	342.0 342.0	3686.0 3686.0	16144.68 16144.68 32289
0310003	Jefferson Smurfit Corp - Jacksonville	439.9 -2100	3359.3 -6300	5 13	175 200	53.3 61.0	10.5 10	3.20 3.05	75 35	22.86 10.67	278 143	409.8 334.8	52.5 373.1	229.77 1634 1864
0310005	Anchor Glass Container Corp.	431.3 -10700	3357.51 -8090	1 2 3 4	57 57 109 117	17.4 17.4 33.2 35.7	3 2.7 5.6 5.2	0.91 0.82 1.71 1.58	64 46 38 39	19.51 14.02 11.58 11.89	461 481 314 460	511.5 522.6 429.8 510.9	34.5 18.3 73.0 54.3	151.24 80 319.92 237.62
0310006	Anheuser Busch, Inc Jacksonville	440.58 -1420	3366.79 1190	1 2 3 4 27 28 31 32	100 100 100 100 100 100 20 20	30.5 30.5 30.5 30.5 30.5 30.5 6.1 6.1	3.5 3.5 3.5 3.5 5.8 5.5 2	1.07 1.07 1.07 1.07 1.77 1.68 0.61 0.61	57.2 57.2 57.2 57.2 64.7 50 6.9 6.9	17.43 17.43 17.43 17.43 19.72 15.24 2.10 2.10	410 410 410 410 285 275 1000 1000	483.2 483.2 483.2 483.2 413.7 408.2 810.9 810.9	36.8 36.8 36.8 75.0 5.2 4.7 4.7	161.18 161.18 161.18 161.18 328.5 22.95 20.8 20.8
0310010	Baptist Medical Centeτ	435.4 -6600	3352.0 -13600	2 3 5 7 8 9 10 11 12 13	39 50 50 35 35 35 35 35 35 50 50	11.9 15.2 15.2 10.7 10.7 10.7 11.9 15.2 15.2	2.5 3 3.5 0.7 0.7 0.7 0.7 2.5 3.5 3.5	0.76 0.91 1.07 0.21 0.21 0.21 0.76 1.07	8.5 150.9 81.2 142 142 142 142 8.5 70.5 84.6	2.59 45.99 24.75 43.28 43.28 43.28 2.59 21.49 25.79	448 325 325 350 350 350 350 448 325 325	504.3 435.9 435.9 449.8 449.8 449.8 504.3 435.9 435.9	6.2 17.1 16.5 22.8 22.8 22.8 22.8 6.2 17.4 22.0	26.98 74.77 72.36 99.96 99.96 99.96 99.96 26.98 76.12 96.36
0310039	Millennium Speciality Chemicals (formerly SCM Glidco Organics)	436.79 -5210	3360.74 -4860	4 5 6 11	40 50 50 45	12.2 15.2 15.2 13.7	3.6 3.6 4 4	1.10 1.10 1.22 1.22	46 42 34 18	14.02 12.80 10.36 5.49	270 505 465 350	405.4 535.9 513.7 449.8	13.0 4.3 18.5 7.3	57 19 81 31.9
0310045	Jacksonville Elect. Auth Northside	447.7 5700	3364.9 -700	1 3 6 7 8 9	250 350 33 33 33 33 240	76.2 106.7 10.1 10.1 10.1 10.1 73.2	16.5 23 19.1 19.1 19.1 19.1 16.5	5.03 7.01 5.82 5.82 5.82 5.82 5.03	65 62 7 7 7 7	19.81 18.90 2.13 2.13 2.13 2.13 1.22	262 330 944 944 944 944 750	400.9 438.7 779.8 779.8 779.8 779.8 672.0	1485.0 1509.8 143.2 143.2 143.2 38.8 65.4	6504.3 6613 627.3 627.3 627.3 170 286.67

Table E-1. Summary of Individual Source Emission and Operating Parameters for the NO<sub>x</sub> AAQS Modeling Analysis

****		Facility Lo		A DIG	g	****	a ~:				-		411 17 330	<b>.</b>
acility ID	Facility None	UTM E,N Relative X,Y		APIS Src #	(ft)	Height	Stack Di		Exit Veloc		Tempe		Allowable NO	
Number 0310046	Facility Name  Jacksonville Elect. Auth Southside		3353.85		144	(m) 43.9	11	(m) 3.35	(ft/s)	(m/s) 11.89	(°F) 305	(K) 424.8	lb/hr 117.8	TPY 516
J310040	Jacksonville Elect. Aum Soumside	437.65		4		44.2			39					
		-4350	-11750	5	145		10	3.05	88	26.82	293	418.2	189.5	830
				10	22	6.7	1.6	0.49	58	17.68	429	493.7	0.7	3
														1349
0310047	Jacksonville Elect. Auth Kennedy	440	3359.2	3	45	13.7	19.1	5.82	11	3.35	826	714.3	3.0	13
0510017	June Diet. Haar. Heinery	-2000	-6400	4	45	13.7	9.1	2.77	52	15.85	826	714.3	22.3	97.76
		-2000	-0400	5	45	13.7	9.1	2.77	52	15.85	826	714.3	22.3	97.70
	•			-										
				6	45	13.7	9.1	2.77	52	15.85	826	714.3	1.1	5
				9	136	41.5	9	2.74	90	27.43	280	410.9	917.7	4019.
				13	33	10.1	1.6	0.49	58	17.68	429	493.7	2.7	11.78
														4245
0310074	U S Gypsum Co	438.9	3361.2	48	88	26.8	1.6	0.49	194.8	59.38	151	339.3	2.3	10
3310074	о о сурзат со	-3100	-4400	55	80	24.4	4	1.22	10.6	3.23	400	477.6	12.5	54.7
		-3100	7400	59	95	29.0	6.7	2.04	5.3	1.62	205	369.3	63.0	
														276
				74	31	9.4	3	0.91	41.1	12.53	315	430.4	0.9	4
				75	30	9.1	3	0.91	51.2	15.61	339	443.7	0.9	4
				76	39	11.9	3.6	1.10	49	14,94	218	376.5	0.9	4
														353
0310180	Amerada Hess Jacksonville	442.7	3365	10	40	12.2	1.5	0.46	37.7	11.49	300	422.0	6.6	29
0310337	Cedar Bay Cogeneration, Inc. b	441.08	3365.06	1	403	122.8	13.3	4.05	120.4	36.70	130	327.6	286.7	1255.0
331033.	Count Day Cogenoration, Inc. o	-920	-540	2	403	122.8	13.3	4.05	120.4	36.70	130	327.6	286.7	1255.
		-720	-540		403	122.8	13.3	4.05	120.4	36.70	130	327.6	286.7	1255.
				3										
				4	63	19.2	4.2	1.28	93.1	28.38	82	300.9	2.4	10.5
				5	63	19.2	4.2	1.28	93.1	28.38	82	300.9	2.4	10.
									•					378
890003	Jefferson Smurfit Corp Fernandina	456.2	3394.2	6	257	78.3	11	3.35	50	15.24	358	454.3	258.0	113
	Beach - (formerly Container Corp.	14200	28600	7	265	80.8	11.5	3.51	61	18.59	428	493.2	45.8	200.7
	of America)	14200	20000	ú	289	88.1	12.7	3.87	62	18.90	411	483.7	51.1	223.
	of America)				340	103.6		4.51	42	12.80	335	441.5	612.6	2683
				15			14.8		42 55					
				21	75	22.9	5.5	1.68	33	16.76	325	435.9	187.2	819. <b>50</b> 5
0890004	Rayonier Inc.	454.7	3392.2	1	180	54.9	10	3.05	32	9.75	145	335.9	28.0	122.6
		12700	26600	2	180	54.9	10	3.05	32	9.75	145	335.9	16.6	72.6
				3	180	54.9	10	3.05	32	9.75	133	329.3	24.9	109
				6	250	76.2	7.5	2.29	57	17.37	125	324.8	291.8	127
				•	223							- · · · ·		158

Notes

Stone Container Facility Location

442.0 3365.6

a Stone Container Facility location is (East, North UTM location (km) are 442.0, 3365.6)

<sup>\*</sup>b NO<sub>X</sub> PSD increment consuming source

Table E-2. Summary of Individual Source Emission and Operating Parameters for the NO<sub>X</sub> AAQS Modeling Analysis

Facility ID	D. W. M	Facility Loc		ISCST3 Source I.D.		Height	Stack Dia		Exit Veloc		Tempera		Allowable NO <sub>X</sub>		Mar	
Number 0310001	Facility Name  Jacksonville Elect. Auth SJRPP	Relative X,Y	700	Name 0310001	(ft) 640 640 640	(m) 195.1 195.1 195.1	(ft) 22.3 22.3 22.3	6.80 6.80 6.80	72.5 72.5 72.5 72.5	22.10 22.10 22.10	(°F) 156 156 156	342.0 342.0 342.0	3686.0 3686.0	464.44 464.44 928.87	M-factor 3,175 3,175	
0310003	Jefferson Smurfit Corp - Jacksonville	-2100	-6300	0310003	175 200 200	53.3 61.0 61.0	10.5 10	3.20 3.05 3.05	75 35 35	22.86 10.67	278 143 143	409.8 334.8 334.8	52.5 373.1	6.61 47.0 <i>i</i> 53.62	75, <b>60</b> 1 4,632	Lowest
0310005	Anchor Glass Container Corp.	-10700	-8090	0310005	57 57 109 117	17.4 17.4 33.2 35.7 33.2	3 2.7 5.6 5.2 5.6	0.91 0.82 1.71 1.58	64 46 38 39	19.51 14.02 11.58 11.89	461 481 314 460 314	511.5 522.6 429.8 510.9	34.5 18.3 73.0 54.3	4.35 2.30 9.20 6.84 22.69	39,843 55,315 17,972 31,685	Lowest
0310006	Anheuser Busch, Inc Jacksonville	-1420	1190	0310006A	100 100 100 100	30.5 30.5 30.5 30.5 30.5	3.5 3.5 3.5 3.5	1.07 1.07 1.07 1.07	57.2 57.2 57.2 57.2 57.2	17.43 17.43 17.43 17.43	410 410 410 410	483.2 483.2 483.2 483.2	36.8 36.8 36.8 36.8	4.64 4.64 4.64 4.64	55,373 55,373 55,373 55,373	
		-1420	1190	0310006B	100 100 100	30.5 30.5 30.5	5.8 5.5 5.8	1.77 1.68 1.77	64.7 50 64.7	19.72 15.24 19.72	285 275 285	413:7 408.2 413.7	75.0 5.2	9.45 0.66 10.11	26,314 287,171	Lowest
		-1420	1190	0310006C	20 20 21	6.1 6.4	2 2 2	0.61 0.61 0.61	6.9 6.9	2.10 2.10 2.10	1000 1000 1000	810.9 810.9 810.9	4.7	0.60 0.60 1.20	17,375 17,375	
0310010	Baptist Medical Center				39 50 50	11.9 15.2 15.2	2.5 3 3.5	0.76 0.91 1.07	8.5 150.9 81.2	2.59 45.99 24.75	448 325 325	504.3 435.9 435.9	6.2 17.1 16.5	0.78 2.15 2.08	20,009 142,063 78,991	Lowest
		-6600	-13600	0310010A	35 35 35 35 35	10.7 10.7 10.7 10.7 10.7	0.7 0.7 0.7 0.7 0.7	0.21 0.21 0.21 0.21 0.21	142 142 142 142 142	43.28 43.28 43.28 43.28 43.28	350 350 350 350 350	449.8 449.8 449.8 449.8 449.8	22.8 22.8 22.8 22.8	2.88 2.88 2.88 2.88 11.50	72,227 72,227 72,227 72,227	
		-6600	-13600	0310010B	39 50 50 39	11.9 15.2 15.2 11.9	2.5 3.5 3.5 2.5	0.76 1.07 1.07 0.76	8.5 70.5 84.6 8.5	2.59 21.49 25.79 2.59	448 325 325 448	504.3 435.9 435.9 504.3	6.2 17.4 22.0	0.78 2.19 2.77 10.75	20,009 65,194 61,800 6 sources	
0310039	Millennium Speciality Chemicals (formerly SCM Glideo Organics)	-5210	-4860	0310039	40 50 50 45 50	12.2 15.2 15.2 13.7	3.6 3.6 4 4	1.10 1.10 1.22 1.22	46 42 34 18	14.02 12.80 10.36 5.49	270 505 465 350 465	405.4 535.9 513.7 449.8 513.7	13.0 4.3 18.5 7.3	1.64 0.55 2.33 0.92	42,260 191,296 34,819 36,886	Lowest
0310045	Jacksonville Elect. Auth Northside	5700 5700	-700 -700	0310045A 0310045B	250 350	76.2 106.7	16.5 23	5.03 7.01	65 62	19.81 18.90	262 330	400.9 438.7	1485.0 1509.8	187.11 190.24	3,235 4,649	
		<i>57</i> 00	-700	0310045C	33 33 33 240 33	10.1 10.1 10.1 10.1 73.2	19.1 19.1 19.1 19.1 16.5	5.82 5.82 5.82 5.82 5.03	7 7 7 7 4	2.13 2.13 2.13 2.13 1.22 2.13	944 944 944 944 750	779.8 779.8 779.8 779.8 672.0	143.2 143.2 143.2 38.8 65.4	18.05 18.05 18.05 4.89 8.25 67.27	927 927 927 927 3,422 7,268	Lowest

Table E-2. Summary of Individual Source Emission and Operating Parameters for the NO<sub>X</sub> AAQS Modeling Analysis

				ISCST3												
Facility ID	<b>-</b>	Facility Loc		Source I.D.		Height	Stack Di		Exit Veloc		Tempe		Allowable NO <sub>X</sub>			
Number	Facility Name	Relative X,Y	(m) a	Name	(ft)	(m)	(ft)	(m)	(ft/s)	(m/s)	(°F)	(K)	lb/hr	g/s	M-factor	
0310046	Jacksonville Elect. Auth Southside				144	43.9	11	3.35	39	11.89	305	424.8	117.8	14.84	14,932	Los
					145	44.2	10	3.05	88	26.82	293	418.2	189.5	23.88	20,761	
					22	6.7	1.6	0.49	58	17.68	429	493.7	0.7	0.09	678,158	
	•	-4350	-11750	0310046	144	43.9	11	3.35	39	11.89	305	424.8		38.81		
0310047	Jacksonville Elect. Auth Kennedy				45	13.7	19.1	5.82	. 11	3.35	826	714.3	3.0	0.37	87,832	
					45	13.7	9.1	2.77	52	15.85	826	714.3	22.3	2.81	55,213	
					45	13.7	9.1	2.77	52	15.85	826	714.3	22.3	2.81	55,213	
					45	13.7	9.1	2.77	52	15.85	826	714.3	1.1	0.14	1,079,534	
					136	41.5	9	2.74	90	27.43	280	410.9	917.7	115.63	4,041	Lo
					33	1.01	1.6	0.49	58	17.68	429	493.7	2.7	0.34	259,059	
	•	-2000	-6400	0310047	136	41.5	9	2.74	90	27.43	280	410.9		122.11		
0310074	U S Gypsum Co				88	26.8	1.6	0.49	194.8	59.38	151	339.3	2.3	0.29	1,878,189	
					80	24.4	4	1.22	10.6	3.23	400	477.6	12.5	1.58	23,889	
					95	29.0	6.7	2.04	5.3	1.62	205	369.3	63.0	7.94	2,175	Lo
					31	9.4	3	0.91	41.1	12.53	315	430.4	0.9	0.12	442,712	
					30	9.1	3	0.91	51.2	15.61	339	443.7	0.9	0.12	550,249	
					39	11.9	3.6	1.10	49	14.94	218	376.5	0.9	0.12	580,871	
		-3100	-4400	0310074	95	29.0	6.7	2.04	5.3	1.62	205	369.3		10.15		
0310180	Amerada Hess Jacksonville	442.7	3365	0310180	40	12.2	1.5	0.46	37.7	11.49	300	422.0	6.6	0.83	71,367	
0310337	Cedar Bay Cogeneration, Inc. b				403	122.8	13.3	4.05	120.4	36.70	130	327.6	286.7	36.12	40,881	
					403	122.8	13.3	4.05	120.4	36.70	130	327.6	286.7	36.12	40,881	
					403	122.8	13.3	4.05	120.4	36.70	130	327.6	286.7	36.12	40,881	
		-198	16	0310337A	403	122.8	13.3	4.05	120.4	36.70	130	327.6		108.37		
					63	19.2	4.2	1.28	93.1	28.38	82	300.9	2.4	0.30	542,871	
					63	19.2	4.2	1.28	93.1	28.38	82	300.9	2.4	0.30	542,871	
		-252	-67	0310337B	63	19.2	4.2	1.28	93.1	28.38	82	300.9		0.60	,	
0890003	Jefferson Smurfit Corp Fernandina				257	78.3	11	3.35	50	15.24	358	454.3	258.0	32.51	16,683	
407000	Beach - (formerly Container Corp.				265	80.8	11.5	3.51	61	18.59	428	493.2	45.8	5.78	128,243	
	of America)				289	88.1	12.7	3.87	62	18.90	411	483.7	51.1	6.44	125,012	
					75	22.9	5.5	1.68	55	16.76	325	435.9	187.2	23.59	7,083	Lo
		14200	28600	0890003A	75	22.9	5.5	1.68	55	16.76	325	435.9		68.31		
		14200	28600	0890003B	340	103.6	14.8	4.51	42	12.80	335	441.5	612.6	77.19	7,588	
0890004	Rayonier Inc.				180	54.9	10	3.05	32	9.75	145	335.9	28.0	3.53	50,936	
					180	54.9	10	3.05	32	9.75	145	335.9	16.6	2.09	85,966	
					180	54.9	10	3.05	32	9.75	133	329.3	24.9	3.14	56,191	
					250	76.2	7.5	2.29	57	17.37	125	324.8	291.8	36.76	11,696	Lo
		12700	26600	0890004	250	76.2	7.5	2.29	57	17.37	125	324.8		45.52		

 $<sup>^{\</sup>circ}$  a Stone Container Facility location is (East, North UTM location (km) are 442.0, 3365.6)  $^{\circ}$ b NO $_{X}$  PSD increment consuming source

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THE FLORIDA TIMES-UNION

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Jacksonville, Fl

Affidavit of Publication
BUREAU OF AIR REGULATION

Florida Times-Union

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R01687

Public Notice Of Int

State of Florida County of Duval

Before the undersigned authority personally appeared Steven L. Smith who on oath says he is a Legal Advertising Representative of The Florida Times-Union, a daily newspaper published in Jacksonville in Duval County, Florida; that the attached copy of advertisement is a legal ad published in The Florida Times-Union. Affiant further says that The Florida Times-Union is a newspaper published in Jacksonville, in Duval County, Florida, and that the newspaper has heretofore been continuously published in Duval County, Florida each day, has been entered as second class mail matter at the post office in Jacksonville, in Duval County, Florida for a period of one year preceeding the first publication of the attached copy of advertisement; and affiant further says that he/she has neither paid nor promised any person, firm or corporation any discount, rebate, commission, or refund for the purpose of securing this advertisement for publication in said newspaper.

PUBLISHED ON: 01/22

FILED ON: 01/22/00

PUBLIC NOTICE OF INTENT TO ISSUE PSD PERMIT
STATE OF FLORIDA
DEPARTMENT OF ENVIRONMENTAL PROTECTION
DEP File No. 0310067-004-AC (PSD-FL-252)
Duval County, Florida

The Department of Environmental Protection (Deportment) gives notice of its intent to issue a permit under the requirements for the Prevention of Significant Deterioration of Air Quality (PSD permit) to Stone Container Corporation. The permit will allow an increase in the maximum steam production rate and heat input rate for each of the three existing package boilers at its Jacksonville Mill in Duval County, Florida. The three package boilers are operated to support the recycled paper mill operations. Each of the three package boilers will increase the steam production rate from 125,000 lb/hr to 150,000 lb/hr, but will maintain the current permitted emission levels for nitrogen oxides (No.) and sulfur dioxide (So<sub>2</sub>).

Maximum heat input rate to each boiler will be 215 MMBtu/hr when firing naturol gas, and 200 MMBtu/hr when firing No. 2 fuel oil. A Best Available Control Technology (BACT) determination was required for NO<sub>X</sub> pursuant to Rule 62-212.400, F.A.C.

The applicant's name and address are Stone Container Corporation, Post office

212.400, F.A.C.

The applicant's name and address are Stone Container Corporation, Post office Box 26998, Jacksonville, Florida 32226-6998. The Jacksonville Mill is located at 9469 East Port Road, Jacksonville, Duval County, Florida.

NOx emissions from the package boilers will be controlled through low-NOx burners and Flue Gas Recirculation.

The net emissions increase due to the increased steam production for RSD applicability purposes is summarized below (in tons per year).

Pollutant

Net Emissions Increase

PSD Significant Emission Röth.

Pollutant NOx Net Emissions Increase 304 PSD Significant Emission Rate

applicability purposes is summarized below (in tons per year).

Pollutant Net Emissions Increase PSD Sianificant Emission Röle\*
NOx 40

An air quality impact analysis was conducted for NOx. Emissions from the facility will not significantly contribute to or cause a violation of any state or federal ambient air quality standards.

The Department will accept written comments and requests for a public meeting concerning the proposed permit issuance action for a period of 30 (thirty) days from the date of publication of this "Public Notice of Intent to Issue PSD permit." Written comments and requests for a public meeting should be provided to the Department's Bureau of Air Regulation at 2600 Blair Stone Road, Mail Station #5505, Tallahassee, Florida 32399-2400. Any written comments filed shall be made available for public inspection.

The Department will issue the permit with the attached conditions unless a timely petition for an administrative hearing is filed pursuant to Sections 120.569 and 120.57 of the Florida Statutes. The petition must contain the information set forth below and must be filed (received) in the Office of General Counsel at the Department, 3900 Commonwealth Boulevard, Mail Station #35, Tallahassee, Florida 23399-3000. Petitions filed by the permit applicant or any of the parties listed below must be filed within fourteen (14) days of receipt of this notice of intent. Petitions filed by any persons other than those entitled to written notice under Section 120.60(3) of the Florida Statutes must be filed within fourteen days of publication of the public notice or within fourteen (14) days of receipt of this notice of intent, whichever occurs first. Under Section 120.60(3), however, any person who asked the Department for notice of agency action may file a petition within fourteen (14) days of receipt of this notice of intent, whichever occurs first. Under Sections 120.569 and 120.57, Florida Statutes, or to intervention will be only at the approval of the perision Ampierative determination (hear

contain the same information as set forth above, as required by Rule 28-106.301 of the Florida Administrative Code.

Because the administrative hearing process is designed to formulate final agency action, the filing of a petition means that the Department's final action may be different from the petition taken by it in this notice. Persons whose substantial interests will be affected by any such final decision of the Department on the application have the right to petition to become a party to the proceeding, in accordance with the requirements set forth above.

A complete project file is available for public inspection during normal business hours, 8:00 a.m. to 5:00 p.m., Monday through Friday, except legal holidays, at:

Department of Environmental Protection
Bureau of Air Regulation
111 South Magnolia Drive, Suite 4
Tallahassee, Florida 32301
Telephone: 850/488-1344

Department of Environmental Protection Northeast District Office 7825 Baymeadows Way, Suite 200B Jacksonville, Florida 32256-7590 Telephone: 904/448-4300

Telephone: 850/488-1344
Fax: 850/722-6979
Fax: 904/448-4300
Fax: 904/448-4366
Regulatory & Environmental Services Department (RESD)
Suite 225, 117 W. Duval Street
Jacksonville, Florida 32202
Telephone: 904/630-3484
Fax: 904/630-3638
The complete project file includes the Draft Permit, the application and the information submitted by the responsible official, exclusive of confidential records under Section 403.111, Florida Statutes. Interested persons may contact the New Resource Review Section at 111 South Magnolia Drive, Suite 4, Tallahassee, Florida 32301, or call 850/488-0114, for additional information.

Name: Steven L. Smith

Title: Legal Advertising Representative

whereof, I have hereunto set my hand and affixed my official

seal, the day and year aforesaid.

Line Week NOTARY :



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## Department of Environmental Protection

Jeb Bush Governor Twin Towers Office Building 2600 Blair Stone Road Tallahassee, Florida 32399-2400

David B. Struhs Secretary

September 10, 1999

#### CERTIFIED MAIL - RETURN RECEIPT REQUESTED

Mr. John L. West, General Manager Stone Container Corporation Post Office Box 26998 Jacksonville, Florida 32226-6998

Re: DEP File No. 0310067-004-AC (PSD-FL-252) Recycled Fiber Facility, Increase in steam rate

Dear Mr. West:

The Regulatory and Environmental Services Department of Jacksonville raised the attached incompleteness issue in regards to the above referenced project. Please respond to their concern as well as to the second incompleteness letter dated September 8, 1999 sent by the Department.

The Department will resume processing this application after receipt of the requested information. If you have any questions regarding this matter, please call Syed Arif, P.E. at (850) 921-9528.

Sincerely,

A. A. Linero, P.E. Administrator New Source Review Section

AAL/sa

#### Enclosure

cc: Doug Neely, EPA

John Bunyak, NPS

- C. Kirts, DEP-NED
- B. Oven, DEP-OSC
- J. Manning, RESD
- D. Roberts, Esq., HGSS
- J. Antista, General Counsel, Fl Game & Fresh Water Fish Commission
- D. Russ, Esq., Dept. of Community Affairs
- E. M. Barker, Esq., Slott & Barker
- L. N. Curtin, Esq., Holland & Knight
- G. K. Radlinski, Esq., City of Jacksonville
- N. B. Barnard, Esq., St. Johns River Water Management District
- R. Vandiver, General Counsel, Fl Public Service Commission

David Buff, Golder Associates Inc.

### REGULATORY & ENVIRONMENTAL SERVICES DEPARTMENT

#### Air and Water Quality Division

September 9, 1999



Mr. Syed Arif, Air Permit Engineer Florida Department of Environmental Protection Bureau of Air Regulation 2600 Blair Stone Road Tallahassee, FL 32399-2400

RE: Duval County - Air Pollution

Stone Container Corporation Permit Modification Request DEP File No. 031-0067-004-AC

Dear Mr. Arif:

The City of Jacksonville, Air and Water Quality Division (AWQD) has reviewed the referenced request dated August 11, 1999 and the stack test results on the three package boilers performed on May 8, 1998. The stack test results indicate the average actual heat input while firing natural gas during the tests on No. 1, No. 2, and No. 3 package boilers was 181 MMBtu/hr., 187 MMBtu/hr. and 172 MMBtu/hr. respectively. The steam production rate during the tests was between 140,000 and 145,000 lb/hr.

The referenced request is asking for an increase in the maximum heat input rate to 215 MMBtu/hr, an increase in steam production rate to 150,000 lb/hr. and to keep the existing allowable NO<sub>x</sub> emission rates of 0.2 lb/MMBtu, 34.94 lb/hr. and 153.1 tons/yr. per boiler. The AWQD believes Stone Container Corporation has not provided reasonable assurance that the three package boilers can demonstrate compliance with the NO<sub>x</sub> emission rates while operating at a heat input rate of 215 MMBtu/hr. The AWQD recommends Florida Department of Environmental Protection request Stone Container Corporation provide additional information providing reasonable assurance the existing allowable NO<sub>x</sub> emission rates can be achieved with a maximum heat input rate of 215 MMBtu/hr, while firing natural gas or No. 2 fuel oil.

Should you have any questions concerning this matter, please contact me at (904) 630-3484.

Very truly yours,

Richard L. Robinson, P.E., Manager Air Pollution Source Permitting Section

RLR/rt

117 West Duval Street, Suite 225 Jacksonville, Florida 32202 Fax (904) 630-3638 Air Quality 630-3484
Water Quality 630-3461
Ground Water 630-4900
Hazardous Materials 630-3404

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6. Signature: (Addressee or Agent)

PS Form 3811, December 1994



Table C-1. Summary of BACT Determinations for NOx from Boilers Fired by Natural Gas

BUCKNELL UNIVERSITY GRAIN PROCESSING CORP. KERN MEDICAL CENTER CALIFORNIA STATE PRISON, CORCORAN DARLING INTERNATIONAL	PA IN CA CA	60-0001A					
KERN MEDICAL CENTER CALIFORNIA STATE PRISON, CORCORAN DARLING INTERNATIONAL	CA		11/26/97	24000 lb/hr Steam	0.1 lb/MMBtu		
CALIFORNIA STATE PRISON, CORCORAN DARLING INTERNATIONAL		CP 027-7239-00046	06/10/97	244 MMBtu/hr	0.05 lb/MMBtu	LOW NOX BURNERS AND FLUE GAS RECIRCULATION (FGR)	
DARLING INTERNATIONAL	CA	S-1678-11-0	01/27/97	3 MMBtu/hr		OPERATION LIMITED TO 80% UTILIZATION. RECORDKEEPING REQUIRED FOR COMPLIANCE	
		C-0214-32-0	01/15/97	8.1 MMBtu/hr	0.012 MMBtu/hr	PREMIXED LEAN BURN COMBUSTION TECHNOLOGY	
THE ACRICO COMPANY FALICTIMA DI ANT	CA	· C-406-3-1	12/30/96	31.2 MMBtu/hr	0.036 lb/MMBtu	LOW-NOX BURNER, FLUE GAS RECIRCULATION (FGR)	_
IMC-AGRICO COMPANY - FAUSTINA PLANT	LA	PSD-LA-602	10/16/96	320 MMBtu/hr	0.08 lb/MMBtu	LOW NOX BURNERS	
O.H. KRUSE GRAIN AND MILLING	CA	S-160-13-0	09/19/96	10 MMBtu/hr	0.106 lb/MMBtu	<del>-</del>	
WEYERHAEUSER COMPANY	MS	1680-44	09/10/96	7 MMBtu/hr	80 PPMVD @ 8% O2	STAGED COMBUSTION	
WEYERHAEUSER COMPANY	MS	1680-44	09/10/96	1600 MMBtu/hr	0.5 lb/MMBtu	CONTINUED EFFICIENT OPERATION WITH LOW NOX BURNERS	
WEYERHAEUSER COMPANY	MS	1680-44	09/10/96	400 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNERS WITH FLUE GAS RECIRCULATION (FGR)	
TOYOTA MOTOR CORPORATION SVCS OF N.A.	IN	CP-051-5391-00037	08/09/96	58 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNERS & FUEL SPEC: USE OF NATURAL GAS 111 AS FUEL	
BOISE CASCADE CORP.	AL	102-1	05/10/96	346.4 MMBtu/hr	0.05 lb/MMBtu	LOW NOX BURNERS AND FLUE GAS RECIRCULATION (FGR)	
MID-GEORGIA COGEN.	GA	4911-76-11753	04/03/96	60 MMBtu/hr	0.1 lb/MMBtu	DRY LOW NOX BURNER WITH FGR	
EXXON COMPANY, USA SANTA YNEZ UNIT PROJECT	CA	ATC-9517	02/05/96	95 MMBtu/hr - each	27 PPMVD AT 3% O2	FLUE-GAS RECIRCULATION (FGR), STEAM INJECTION	
SITIX OF PHOENIX, INC.	ΑZ	950460	02/01/96	42 MMBtu/hr	49 TPY	FLUE GAS RECIRCULATION (FGR)-NOX NOT TO EXCEED 30 PPM	
MINNESOTA CORN PROCESSORS	MN	8300038-19	08/09/95	• •	24.1 lb/hr	USE OF LOW NOX MULTISTAGE COMBUSTION COMBINED WITHINDUCED FLUE GAS RECIRCULATION (FGR)	
GEORGIA PACIFIC CORP. (MONTICELLO MILL)	MS	1500-7	07/11/95	776 MMBtu/hr	, <del></del>	NO PHYSICAL MODIFICATION TO BOILER. BACT NOT REQUIRED.	
TRANSAMERICAN REFINING CORPORATION	LA	PSD-LA-571 (M-1)	02/10/95	244 MMBtu/hr	19.8 lb/hr	LOW NOX BURNERS/COMBUSTION CONTROL	
KAMINE/BESICORP SYRACUSE LP	NY	313201 2010/00001-00007	12/10/94	2.5 MMBtu/hr	0.12 lb/MMBtu	and a <del>-</del> Caramana and Angles and	-
KAMINE/BESICORP SYRACUSE LP	NY	313201 2010/00001-00007	12/10/94	33 MMBtu/hr	0.035 lb/MMBtu	INDUCED FLUE GAS RECIRCULATION (FGR)	70.9
COURTAULDS FIBERS, INC.	AL	503-5002-X023 AND -X24	11/02/94	148 MMBtu/hr	10.4 lb/hr	LOW NOX BURNERS WITH 8% FLUE GAS RECIRCULATION	87
JVC MAGNETICS AMERICA CO.	AL	413-0040-X001,X002,X003,X006	06/16/94	5.2 MMBtu/hr	40 TPY	FUEL SPEC: NATURAL GAS W/ MAX 0.5% SULFUR FUEL OILAS BACKUP	
PORTLAND GENERAL ELECTRIC CO.	OR	25-31	05/31/94	361 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNER AND FLUE GAS RECIRCULATION	-
INTEL CORPORATION	ΑZ	93-46	04/10/94	50 MMBtu/hr		LOW NOX BURNERS	
CHAMPION INTERNATIONAL CORP	FL	PSD-FL-200	03/25/94	533 MMBtu/hr	0.06 lb/MMBtu	COEN LOW NOX BURNERS AND FGR	
STAFFORD RAILSTEEL CORPORATION	AR	1471-A	08/17/93	46.5 MMBtu/hr	7.1 TPY	FUEL SPEC: USE OF NATURAL GAS & LOW NOX BURNERS	
LOCKPORT COGEN FACILITY ANITEC COGEN PLANT	NY NY	292600 0446/00001-00007	07/14/93	210 MMBtu/hr	0.2 lb/MMBtu	<del></del>	
NEWARK BAY COGENERATION PARTNERSHIP, L.P.		030200 0451 01-92-5231 TO 01-92-5261	07/07/93	123 MMBtu/hr	0.05 lb/MMBtu		
NEWARK BAY COGENERATION PARTNERSHIP, L.P.	NJ	01-92-5231 TO 01-92-5261	06/09/93	206 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNERS, FLUE GAS RECIRCULATION (FGR)	
INDECK ENERGY COMPANY	NY	563203 0099	06/09/93	200 MMBtu/hr	0.05 lb/MMBtú	LOW NOX BURNERS, FLUE GAS RECIRCULATION (FGR)	
CNG TRANSMISSION CORPORATION	W	R13-1471/R14-9	05/12/93 05/03/93	0 MMBtu/hr	0.2 lb/MMBtu 140 LB/MM cu ft	-	
INDELK ENERGY SERVICES OF OTSEGO	MI	143-90	03/16/93	10 MMBtu/hr 778 MMBtu/hr	0.25 lb/MMBtu	SNCR/DRY CONTROL	50
INDELK ENERGY SERVICES OF OTSEGO	MI	143-90	03/16/93	99 MMBtu/hr	0.25 lb/MMBtu	FLUE GAS RECIRCULATION	40
TRANSAMERICAN REFINING CORPORATION (TARC)	LA	PSD-LA-571	01/15/93	1.2 MMBtu/hr	0.14 lb/hr	" GOOD COMBUSTION PRACTICES	
AMERICAN CRYSTAL SUGAR COMPANY	MN	29B-92-OT-1	12/15/92	200.1 MMBtu/hr	0.075 lb/MMBtu	LOW NOX BURNER WITH FLUE GAS RECIRCULATION BOILER INSTALLATION	
KAMINE/BESICORP CORNING L.P.	NY	8-4638-22/1-0	11/05/92	33.5 MMBtu/hr	0.32 lb/MMBtu	LOW NOX BURNER, FGR	
SUNLAND REFINERY	CA	S-0207-0085-00 & -0036-00	09/24/92	12.6 MMBtu/hr	0.036 lb/MMBtu	FGR/LOW NOX BURNER	_
CPC - CORN PRODUCTS DIVISION	IL	91020069/ID 031012ABI	08/06/92	600 MMBtu/hr	0.05 lb/MMBtu	LOW NOX BURNER & FLUE GAS RECIRCULATION	85
SARANAC ENERGY COMPANY	NY	5-942-106/1-9	07/31/92	249 MMBtu/hr	0.136 lb/MMBtu	LOW NOX BURNERS	
INDECK-YERKES ENERGY SERVICES	NY	146400 0133	06/24/92	99 MMBtu/hr	0.2 lb/MMBtu	EOW HOX BUILD	
BOISE CASCADE CORPORATION	AL	102-1	04/01/92	343.4 MMBtu/hr	0.05 lb/MMBtu	_	_
BERMUDA HUNDRED ENERGY LIMITED PARTNERSHIP	VA	51020	03/03/92	250 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNER	_
KALAMAZOO POWER LIMITED	MI	1234-90	12/03/91	500 KW	0.02 lb/MMBtu	EOW NOX BONNER	
SCOTT PAPER COMPANY	AL	503-2012	09/17/91	220.5 MMBtu/hr	0.1 lb/MMBtu	FACILITY NOW SHUT DOWN.	
JAMES RIVER CORP	MI	423-91	09/17/91	226.7 MMBtu/hr	0.06 lb/MMBtu	LOW NOX BURNERS AND FGR SYS	70
MINNESOTA CORN PROCESSORS, INC.	MN	AMENDMENT 6 TO 1939-88-0T-1	06/25/91	178.7 MMBtu/hr	0.125 lb/MMBtu	LOW NOX BURNERS	
CHAMPION INTERNATIONAL	AL	707-1-U54	05/08/91	5.8 MMBtu/hr	0.05 lb/MMBtu	FLUE GAS RECIRCULATION	
NORTHERN CONSOLIDATED POWER	PA	25-328-1	05/03/91	100.4 MMBtu/hr	0.1 lb/MMBtu		_
LAKEWOOD COGENERATION, L.P.	NJ	25 520-1	04/01/91	131 MMBtu/hr	0.2 lb/MMBtu	LOW NOX BURNERS	50
LAKEWOOD COGENERATION, L.P.	NJ	· <del>_</del>	04/01/91	131 MMBtu/hr	0.1 lb/MMBtu	LOW NOX BURNERS	50
DEL MONTE FOODS, USA	CA	304000000	09/26/90	20.9 MMBtu/hr	40 PPMVD @ 3% O2	BURNER, JOHNSTON	_
I/N KOTE	IN	PC (71) 1822	11/20/89	70.8 MMBtu/hr	0.05 lb/MMBtu	FUEL SPEC: USE OF NATURAL GAS & FLUE GAS RECIRC ULATION (FGR)	
GENERAL ELECTRIC CO.	IN	PSD (65) 1757	09/17/89	93 MMBtu/hr	0.133 lb/MMBtu	STAGED COMBUSTION AIR & LOW EXCESS AIR	_
GENERAL ELECTRIC CO.	IN	PSD (65) 1757	09/17/89	250 MMBtu/hr	0.12 lb/MMBtu	LOW NOX BURNERS, STAGED COMBUSTION AIR	

Source: EPA's RACT/BACT/LAER Clearinghouse, 1998

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