

ENVIRONMENTAL SERVICES

4014 NW THIRTEENTH STREET
GAINESVILLE, FLORIDA 32609
352/377-5822 ■ FAX/377-7158

TESTS 10/9/2001

KA 263-00-09

January 17, 2001

Mr. Al Linero
Florida Department of
Environmental Protection
2600 Blair Stone Road
Tallahassee, FL 32399-2400

Subject: Air Emission Measurements Report
Miami Cement Plant
1200 NW 137th Avenue
Permit No. 0250014-002-AC

Dear Mr. Linero:

Enclosed is a copy of our report describing the results of particulate matter emissions measurements conducted September 29, 2000, at the subject facility. A copy of our report describing the results of sulfur dioxide, nitrogen oxides and carbon monoxide emission measurements conducted October 9, 2000, was hand delivered to you on January 16, 2001.

If you have any questions, please do not hesitate to contact me.

Very truly yours,

KOOGLER & ASSOCIATES

John B. Koogler, Ph.D., P.E.

JBK:wa
Enc.

C: Mr. Michael Vardeman, Rinker

TESTS
10/9/2001

SULFUR DIOXIDE, NITROGEN OXIDES AND
CARBON MONOXIDE EMISSION
MEASUREMENTS

KILN/RAW MILL/CLINKER COOLER

CSR RINKER MATERIALS CORPORATION
MIAMI, FLORIDA

PERMIT NO. 0250014-002-AC

TEST DATE: OCTOBER 9, 2000

RECEIVED

JAN 16 2001

BUREAU OF AIR REGULATION



KOOGLER & ASSOCIATES

ENVIRONMENTAL SERVICES

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CARBON MONOXIDE EMISSION MEASUREMENTS

KILN/RAW MILL/CLINKER COOLER

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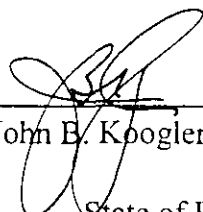
PERMIT NO. 0250014-002-AC

TEST DATE: OCTOBER 9, 2000

KOOGLER & ASSOCIATES
ENVIRONMENTAL SERVICES
4014 N.W. 13TH STREET
GAINESVILLE, FLORIDA 32609
(352) 377-5822



To the best of my knowledge, all applicable field and analytical procedures comply with the Florida Department of Environmental Protection requirements and all test data and plant operating data are true and correct.



John B. Koogler, Ph.D., P.E.
State of Florida
Registration No. 12925

12/14/00
Date



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1.0 INTRODUCTION

CSR Rinker Materials Corporation owns and operates a preheater/precalciner Portland cement plant at 1200 NW 137th Avenue, Miami, Dade County, Florida. On October 9, 2000, Koogler & Associates Environmental Services of Gainesville, Florida, conducted sulfur dioxide, nitrogen oxides, and carbon monoxide emission measurements on the kiln/raw mill/cooler in accordance with EPA Methods 6C, 7E, and 10 (40 CFR 60, Appendix A). The purpose of the testing was to demonstrate initial compliance with the emission limiting standards set forth in Permit No. 0250014-002-AC.

Prior to the test date, the Metropolitan Dade County Environmental Resources Management in Miami, Florida, was notified of the scheduled initial air emission performance tests.

During the period of testing, the plant was operating normally at a preheater feed rate of 172.3 tons per hour and a clinker production rate of 103.4 tons per hour. The coal feed rate averaged 13.0 tons per hour which is equivalent to a heat input rate of about 325 MMBtu/hr. The permitted preheater feed rate and clinker production rates are 220 tons per hour and 137 tons per hour, respectively, on a 24-hour basis and limits the heat input rate to 437 MMBtu/hr. The sulfur dioxide emission rate averaged 2.85 pounds per hour, the nitrogen oxides emission rate

averaged 339.19 pounds per hour; and the carbon monoxide emission rate averaged 249.97 pounds per hour. The permit limits the sulfur dioxide emission rate to 228 pounds per hour, the nitrogen oxides emission rate to 497 pounds per hour, and the carbon monoxide emission rate to 311 pounds per hour at the tested operating rate.

Based upon the data presented herein, it can be concluded that during the period of testing on October 9, 2000, the kiln/raw mill/cooler were operating in compliance with the SO₂, NO_x, and CO standards set forth in Permit 0250014-002-AC.

2.0 LOCATION OF SAMPLING PORTS

The locations of the sampling points are shown in Figure 1. Stack gas flow rate measurements were made through four sampling ports located 90 degrees to one another in the 136.5-inch diameter stack. The ports are located 203.5 feet (18.5 diameters) above the point where the stack gas enters the stack and 101.7 feet (9.3 diameters) below the top of the stack. A total of 12 sampling points were used for the velocity and sampling traverses. The sampling points were located in accordance with criteria established by EPA Test Method 1 (40 CFR 60, Appendix A).

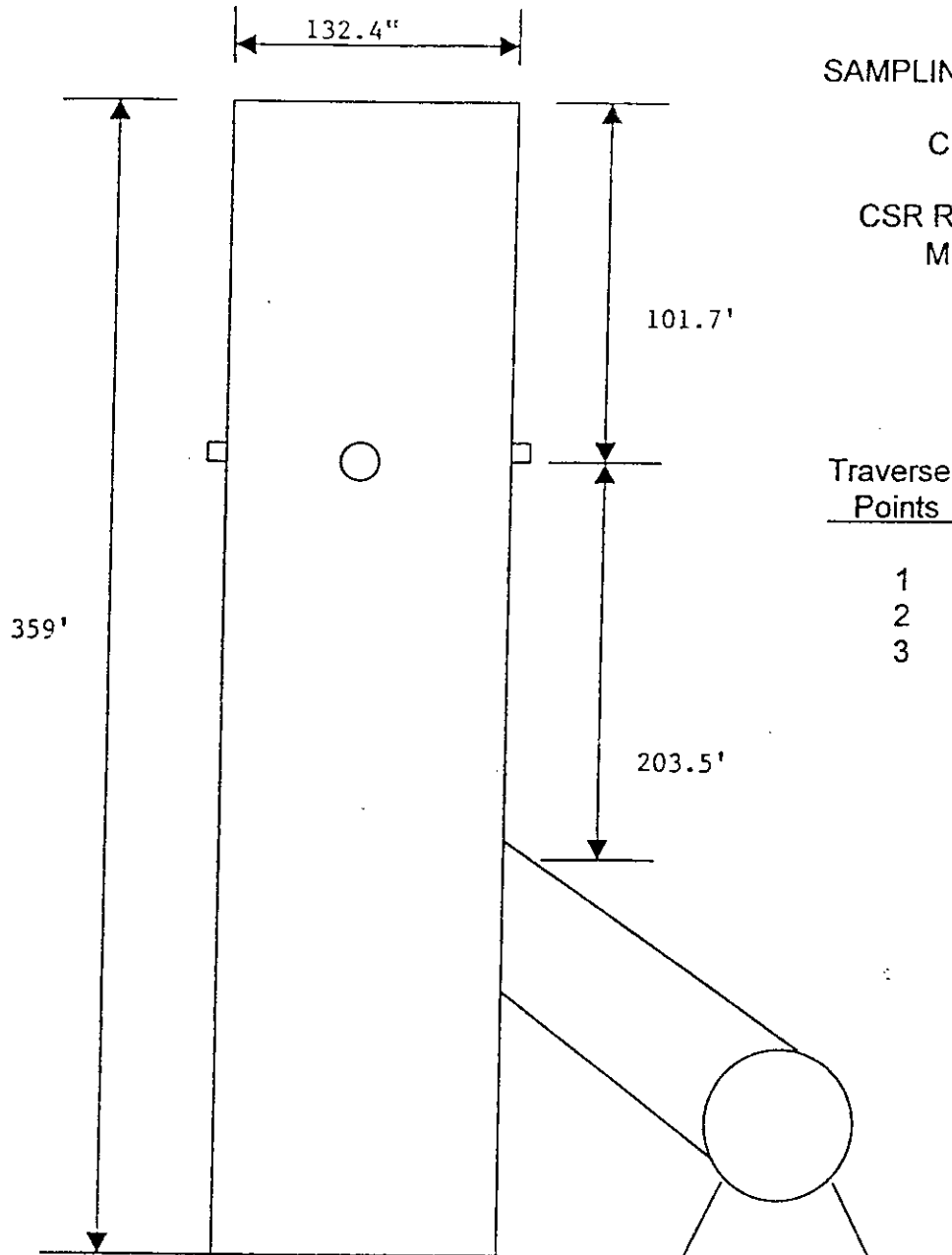
Samples for measurements of nitrogen oxides (Method 7E), carbon monoxide (Method 10) and sulfur dioxide (Method 6C) were collected from a single point near the center of the stack.

FIGURE 1

SAMPLING POINT LOCATIONS

CEMENT PLANT

CSR RINKER MATERIALS
MIAMI, FLORIDA



<u>Traverse Points</u>	<u>Distance from Inside Stack Wall</u>
1	6.01
2	19.9
3	40.4

3.0 FIELD AND ANALYTICAL PROCEDURES

The SO₂, NO_x and CO emission measurements were made using EPA Methods 6C, 7E and 10, respectively. The sample of stack gas for the continuous analyzers was collected from a single point near the center of the stack and transported to a heated manifold through a heated teflon sample line. The sample gas stream was split with the fractions for NO_x and SO₂ analyses passing through a cold trap to remove water vapor before the gas streams were introduced to the respective analyzers. The gas sample for carbon monoxide analysis was passed through an ascarite column to remove moisture and CO₂. Stack gas velocity measurements and stack gas moisture measurements were made in accordance with EPA Methods 2 and 4.

All EPA test methods are described in 40 CFR 60, Appendix A and have been adopted by reference by FDEP by Rule 62-297.401, F.A.C.

4.0 SUMMARY OF RESULTS

Results of the sulfur dioxide, nitrogen oxides and carbon monoxide emission measurements are summarized in Table 1. During the test period, the sulfur dioxide emission rate averaged 2.85 pounds per hour as measured by EPA Method 6C, the nitrogen oxides emission rate averaged 339.19 pounds per hour as measured by EPA Method 7E and the carbon monoxide emission rate averaged 249.97 pounds per hour as measured by EPA Method 10. The permit limits the sulfur dioxide emission rate to 0.7 pounds per MMBtu or to 228 pounds per hour at test conditions, the nitrogen oxides emission rate 1.53 pounds per MMBtu (497 pounds per hour) and carbon monoxide emission rate to 3.01 pounds per ton of clinker (311 pounds per hour).

Based upon the data presented herein, it can be concluded that during the period of testing on October 9, 2000, the kiln/raw mill/cooler were operating in compliance with the SO₂, NO_x and CO standards set forth in Permit 0250014-002-AC.

Emission calculations, field and laboratory data sheets, plant information, equipment calibrations, and a list of project participants are included in the Appendix of this report.

TABLE 1

SUMMARY OF CO, SO₂, AND NO_x EMISSION MEASUREMENTS

CSR RINKER
 KILN/RAW MILL/COOLER
 OCTOBER 9, 2000

Run No.	CO		SO ₂		NO _x	
	ppm	lb/hr	ppm	lb/hr	ppm	lb/hr
1	302.36	253.99	1.83	1.66	249.24	336.45
2	321.73	273.53	2.48	3.34	236.24	320.52
3	263.16	222.39	2.92	3.54	274.20	360.59
Avg	295.75	249.97	2.41	2.85	253.23	339.19

Calculations: CO, SO₂, NO_x

$$\text{lb/hr} = \text{ft}^3/\text{min} \times 60 \text{ min/hr} \times (\text{conc. ppm}) \times \text{MW}/385 \times 10^{-6}$$

Run	(dscfm)
1	190,765
2	194,765
3	190,613

APPENDIX



CALCULATIONS



j::

Company: CSR Rinker
Source: Cement plant - Run 1

Location: Miami, FL
Date: 10/9/00

vs =	51.34	FT/SEC	As =	95.61	ft^2
Q =	294518	acfm -			not corrected
Q(std) =	190765	dscfm -			both temperature and moisture corrected
Q(moist) =	255076	dcfm -			only moisture corrected
Q(temp) =	221820	scfm -			only temperature corrected

Moisture

Vm(Std) =	46.1097867	Bws =	0.0959763	Lower Bws
Vw(Std) =	4.89528	Bws @sat =	1	Value used
		Percent Moist =	9.5976347	

Emission Rates:	CO =	253.99	lb/hr	
	NOx =	336.45	lb/hr	as NO2
	SO2 =	1.66	lb/hr	
	THC =	0.00		as Propane

EQUATIONS :

$$As = (PI*(Stack\ Dia/12)^2)/4 \quad \text{--- Round Stacks}$$

or

$$As = (Stack\ L/12)*(Stack\ W/12) \quad \text{--- Square Stacks}$$

$$Md = (.44*\%CO2)+(.32*\%O2)+(.28*(100-(\%CO2+\%O2)))$$

$$Ms = (Md*(1-\%Moist))+(.18*\%Moist)$$

$$P(stack) = Pb+(Ps/13.6)$$

$$vs = (85.49)*(0.85)*(Sqrt.Dp)*(Sqrt[(T(s)+460)/(Ms*P(stack))])$$

$$Q = vs * As * 60$$

$$Q(std) = Q*(1-\%Moist)*(528/(Ts+460))*(P(stack)/29.92)$$

$$Vm (Std) = 17.6471 * Vm * Y * ((Pb+(dH/13.6))/(Tm+460))$$

$$Vw (Std) = 0.0471 * Vlc$$

$$Bws = (Vw(Std) / (Vm(Std)+ Vw(Std))$$

$$Bws @ Sat = \text{Vap. Pressure of H2O @ Dew Point Temp}/Ps$$

$$CO (lb/hr) = ((PPM CO)*Q(std)*28.01*60)/(385*10^6)$$

$$NOx (lb/hr) = ((PPM NOx)*Q(std)*46.006*60)/(385*10^6)$$

$$SO2 (lb/hr) = ((PPM SO2)*Q(std)*64.0648*60)/(385*10^6)$$

$$THC (lb/hr) = ((PPM THC)*Q(temp)*44.0965*60)/(385*10^6)$$

Company: CSR Rinker
Cement plant - Run 1

Location: Miami, FL
Date: 10/9/00

Sqrt.Dp= 0.7800
T(s)= 245.00

12
Filename:
QuickFLOW
[Alt-C]
to clear input
range

Data Point	Stack Velocity Head	Stack Gas Temp.
1	0.66	246
2	0.64	246
3	0.45	246
4	0.70	246
5	0.67	246
6	0.51	246
7	0.69	246
8	0.66	246
9	0.50	246
10	0.69	246
11	0.66	246
12	0.51	246
13	0.00	0
14	0.00	0
15	0.00	0
16	0.00	0
17	0.00	0
18	0.00	0
19	0.00	0
20	0.00	0
21	0.00	0
22	0.00	0
23	0.00	0
24	0.00	0
25	0.00	0
26	0.00	0
27	0.00	0
28	0.00	0
29	0.00	0
30	0.00	0
31	0.00	0
32	0.00	0
33	0.00	0
34	0.00	0
35	0.00	0
36	0.00	0

Pb = 30.18 in Hg
Ps = -0.66 in H2O
%O2 = 13.77 %
%CO2 = 5.93 %
%Moist = 14.00 %
Stack Dia= 132.4 in
or
Stack L = in
Stack W = in
PPM CO = 305.01 ppm
PPM NOx = 245.99 ppm
PPM SO2 = 0.87 ppm
PPM THC = 0 ppm
Vm = 47.31 ft3
dH = 1.84 in H2O
Tm = 90 F
Y = 1.002
Vlc = 104 ml

TEST START DATE: 10/9/2000
 TEST START TIME: 10:13
 TEST LOCATION: RINKER RUN 1
 EMPLOYEE NAME: ---
 EMPLOYEE NUMBER: ---
 DEPARTMENT: ---
 COMMENT FIELD 1: O2 SPAN = 25 %, SO2 SPAN = 100 PPM
 COMMENT FIELD 2: NOX SPAN = 1000 PPM, CO SPAN = 1000 PPM
 NUMERIC CODES: --- --- --- --- ---

METROSONICS dl-714 SN 1554 V2.3 07/91

CURRENT DATE: 10/09/00
 CURRENT TIME: 11:43:37

TEST STARTING DATE: 1/ 1/86
 TEST STARTING TIME: 0:37:41

ELAPSED TIME: 0 DAYS 2:46:28
 SAMPLE RATE: 1/sec

TIME	AVG CH 1 % O2	AVG CH 2 PPM SO2	AVG CH 3 PPM NOX	AVG CH 4 PPM CO	
1/ 1/86					
0:37:41	20.56	2.59	0.00	6.73	
0:38:41	20.55	2.25	0.00	6.39	
0:39:41	20.54	2.23	0.00	6.06	
0:40:41	20.52	2.15	0.00	6.06	
0:41:41	20.52	1.62	0.00	6.06	
0:42:41	20.51	1.57	0.00	6.28	<<< ZERO AIR
0:43:41	20.50	1.16	0.00	6.51	
0:44:41	20.49	2.21	0.00	74.37	
0:45:41	20.48	45.04	310.23	509.70	
0:46:41	18.25	49.52	470.30	521.48	
0:47:41	4.86	49.46	470.85	521.14	<<< 45.49 PPM SO2, 473 PPM NOX
0:48:41	2.85	49.72	471.40	521.71	517 PPM CO
0:49:41	3.78	40.34	550.06	622.66	
0:50:41	3.54	41.22	919.69	858.10	
0:51:41	2.84	63.86	933.44	857.43	
0:52:41	2.54	73.77	931.24	852.50	
0:53:41	2.49	78.25	930.69	851.49	
0:54:41	2.46	89.77	930.69	852.94	
0:55:41	2.44	94.48	931.79	851.37	<<< 95.46 PPM SO2, 855 PPM CO
0:56:41	2.44	94.80	932.34	851.60	941 PPM NOX
0:57:41	2.48	95.81	932.34	705.66	
0:58:41	12.83	95.23	765.13	33.09	
0:59:41	19.88	79.23	7.70	11.67	
1: 0:41	20.32	51.81	4.95	10.88	

1: 1:41	20.38	4.03	3.85	10.88	
1: 2:41	20.40	2.30	3.30	10.32	
1: 3:41	20.44	2.17	3.30	10.10	
1: 4:41	20.49	2.37	2.75	9.98	
1: 5:41	20.52	2.50	2.75	9.09	
1: 6:41	20.53	5.90	1.65	9.42	<<< SYSTEM
1: 7:41	20.67	1.76	2.20	5.38	
1: 8:41	20.84	0.13	1.10	5.05	
1: 9:41	20.87	0.20	0.55	4.71	
1:10:41	20.88	0.02	0.55	4.60	<<< ZERO AIR
1:11:41	20.88	2.09	0.55	4.49	
1:12:41	20.88	1.67	0.55	41.28	
1:13:41	12.44	1.97	0.55	433.31	
1:14:41	7.05	2.39	0.55	426.47	
1:15:41	3.60	1.88	0.55	507.24	
1:16:41	2.67	2.11	0.55	508.36	
1:17:41	2.55	1.78	0.55	509.03	<<< 517 PPM CO
1:18:41	2.51	1.71	0.55	508.24	
1:19:41	2.73	1.33	1.10	217.39	
1:20:41	2.66	2.39	1.65	6.95	
1:21:41	2.45	2.07	1.10	4.71	
1:22:41	2.49	1.88	323.43	5.50	
1:23:41	2.60	22.67	475.80	4.60	
1:24:41	2.45	109.55	477.45	4.37	
1:25:41	2.43	INVALID	476.35	4.37	<<< 473 PPM NOX
1:26:41	2.45	INVALID	470.85	4.49	
1:27:41	2.47	114.54	72.06	4.49	
1:28:41	2.46	80.75	2.75	5.05	
1:29:41	2.37	49.81	2.20	4.71	<<< 45.49 PPM SO2
1:30:41	2.39	37.44	1.65	4.60	
1:31:41	2.39	30.42	1.65	4.60	
1:32:41	5.10	25.70	49.51	7.74	
1:33:41	16.10	20.20	247.52	227.71	
1:34:41	13.72	14.29	248.07	319.80	
1:35:41	13.41	10.66	257.98	293.66	
1:36:41	13.41	8.45	268.98	286.15	
1:37:41	13.34	6.64	266.78	276.95	
1:38:41	13.36	5.17	269.53	282.89	
1:39:41	13.41	4.34	275.58	283.12	
1:40:41	13.42	3.64	282.18	284.46	
1:41:41	13.40	2.80	285.48	270.33	
1:42:41	13.41	2.66	280.53	274.14	
1:43:41	13.43	1.95	282.18	269.66	
1:44:41	13.40	1.37	282.18	261.02	<<< STACK
1:45:41	13.38	1.21	276.68	277.51	
1:48:41	13.35	0.89	275.03	281.10	
1:47:41	13.36	0.74	274.48	278.30	
1:48:41	13.38	0.49	273.38	276.28	
1:49:41	13.36	0.49	271.73	282.45	
1:50:41	13.31	0.35	271.18	293.21	
1:51:41	13.29	-0.12	268.43	290.30	

1:52:41	13.30	0.22	266.78	280.31	
1:53:41	13.25	0.75	271.73	266.74	
1:54:41	13.24	3.08	287.68	268.98	<<< START RUN 1
1:55:41	13.25	2.78	283.83	262.59	
1:56:41	13.34	2.36	292.63	264.83	
1:57:41	13.39	2.49	297.58	268.98	
1:58:41	13.40	2.14	294.28	269.99	
1:59:41	13.35	2.21	291.53	277.85	
2: 0:41	13.36	2.22	281.63	279.98	
2: 1:41	13.37	1.97	275.03	282.89	
2: 2:41	13.33	2.06	268.43	286.15	
2: 3:41	13.31	2.09	261.28	298.26	
2: 4:41	13.31	1.86	270.63	287.94	
2: 5:41	13.26	1.78	267.88	284.46	
2: 6:41	13.21	1.66	267.86	286.15	
2: 7:41	13.19	1.63	273.38	287.16	
2: 8:41	13.19	1.93	268.43	295.91	
2: 9:41	13.16	1.73	261.28	299.16	
2:10:41	13.17	1.47	259.63	308.58	
2:11:41	13.17	1.54	260.73	303.76	
2:12:41	13.16	1.32	254.68	316.43	
2:13:41	13.16	1.16	245.87	332.81	
2:14:41	13.16	1.23	239.27	317.22	
2:15:41	13.17	1.33	241.47	321.03	
2:16:41	13.18	1.35	240.92	323.95	
2:17:41	13.22	1.35	233.22	325.41	
2:18:41	13.25	1.12	233.77	307.91	
2:19:41	13.28	1.76	238.72	287.38	
2:20:41	13.32	2.25	238.72	287.61	
2:21:41	13.30	2.53	244.77	291.08	
2:22:41	13.29	2.07	246.97	295.91	
2:23:41	13.31	2.39	242.57	301.51	
2:24:41	13.31	2.27	239.27	303.98	
2:25:41	13.30	2.05	237.62	313.18	
2:26:41	13.28	2.07	242.57	298.60	
2:27:41	13.27	1.88	248.07	293.33	
2:28:41	13.27	1.90	247.52	293.89	
2:29:41	13.28	2.20	245.87	294.78	
2:30:41	13.28	2.10	242.57	300.95	
2:31:41	13.30	1.93	242.02	311.83	
2:32:41	13.27	1.98	234.87	317.78	
2:33:41	13.25	1.77	239.82	306.23	
2:34:41	13.25	1.75	236.52	301.29	
2:35:41	13.22	1.46	233.77	316.99	
2:36:41	13.15	1.66	233.77	329.44	
2:37:41	13.15	1.52	234.32	326.30	
2:38:41	13.15	1.47	229.92	322.60	
2:39:41	13.17	1.52	228.27	323.16	
2:40:41	13.19	1.56	227.72	320.92	
2:41:41	13.26	1.65	228.82	324.40	
2:42:41	13.30	1.59	237.07	309.48	

2:43:41	13.32	1.68	242.57	304.66	
2:44:41	13.33	1.52	238.72	309.70	
2:45:41	13.37	1.29	231.57	304.21	
2:46:41	13.36	1.63	227.17	312.51	
2:47:41	13.39	1.25	232.67	301.40	
2:48:41	13.39	1.66	239.27	297.25	
2:49:41	13.36	1.79	236.52	307.68	
2:50:41	13.32	1.83	232.12	318.45	
2:51:41	13.33	1.99	232.12	316.66	
2:52:41	13.33	1.83	237.07	320.13	
2:53:41	13.30	1.89	239.82	314.86	
2:54:41	13.27	1.95	238.72	305.66	<<< END RUN 1
2:55:41	13.23	1.78	237.07	305.44	
2:56:41	13.22	1.86	240.92	313.07	
2:57:41	13.29	1.74	103.41	242.85	
2:58:41	17.49	1.41	4.95	20.30	
2:59:41	20.15	0.90	3.30	3.37	
3: 0:41	20.33	0.69	2.75	3.25	<<< ZERO AIR
3: 1:41	20.61	0.80	2.20	3.14	
3: 2:41	20.83	0.23	1.65	6.62	
3: 3:41	16.59	0.33	1.65	346.49	
3: 4:41	4.22	0.41	1.65	508.81	
3: 5:41	2.68	0.41	1.65	511.27	
3: 6:41	2.55	0.32	1.10	511.83	<<< 517 PPM CO
3: 7:41	2.47	0.09	1.10	511.39	
3: 8:41	2.38	-0.11	43.45	510.38	
3: 9:41	2.36	0.02	449.40	189.12	
3:10:41	2.28	0.07	478.55	4.60	
3:11:41	2.27	-0.25	478.55	3.03	<<< 473 PPM NOX
3:12:41	2.25	-0.20	479.65	2.80	
3:13:41	2.29	25.53	385.59	2.80	
3:14:41	6.75	47.41	29.15	6.28	
3:15:41	18.48	47.02	3.85	7.63	<<< 45.49 PPM CO
3:16:41	20.25	47.15	2.75	7.29	
3:17:41	20.44	40.87	2.20	7.52	
3:18:41	20.59	0.61	1.10	4.04	
3:19:41	20.78	1.32	1.10	3.03	
3:20:41	20.81	1.28	1.10	3.03	
3:21:41	20.83	1.22	99.01	36.34	
3:22:41	17.03	1.57	225.52	312.06	
3:23:41	13.70	1.54	227.72	324.96	
AVERAGE	13.27	1.83	249.24	302.36	
CO2 =	5.93	%			
O2 =	11.77	%			

CEM BIAS CORRECTION

ANALYZER RESPONSE	ZERO BIAS	SPAN GAS VALUE	SPAN GAS CORRECTED ANALYZER EFFLUANT RESPONSIVE VALUE
302.36 CO	4.05	516.80	509.50 305.01
1.83 SO2	0.96	45.49	46.04 0.87
249.24 NOX	1.90	473.00	477.50 245.99

Company: CSR Rinker
Cement plant - Run 2

Location: Miami, FL
Date: 10/9/00

Sqrt.Dp= 0.7796

T(s)= 246.00

12

Filename:
QuickFLOW
[Alt-C]
to clear input
range

Data Point	Stack Velocity Head	Stack Gas Temp.	
1	0.71	246	Pb = 30.18 in Hg
2	0.62	246	Ps = -0.7 in H2O
3	0.48	246	%O2 = 13 %
4	0.70	246	%CO2 = 5.18 %
5	0.66	246	%Moist = 12.00 %
6	0.52	246	Stack Dia= 132.4 in
7	0.68	246	or
8	0.67	246	Stack L = in
9	0.53	246	Stack W = in
10	0.69	246	PPM CO = 321.73 ppm
11	0.59	246	PPM NOx = 229.53 ppm
12	0.48	246	PPM SO2 = 1.72 ppm
13	0.00	0	PPM THC = 0 ppm
14	0.00	0	Vm = 47.31 ft3
15	0.00	0	dH = 1.84 in H2O
16	0.00	0	Tm = 90 F
17	0.00	0	Y = 1.002
18	0.00	0	Vlc = 104 ml
19	0.00	0	
20	0.00	0	
21	0.00	0	
22	0.00	0	
23	0.00	0	
24	0.00	0	
25	0.00	0	
26	0.00	0	
27	0.00	0	
28	0.00	0	
29	0.00	0	
30	0.00	0	
31	0.00	0	
32	0.00	0	
33	0.00	0	
34	0.00	0	
35	0.00	0	
36	0.00	0	

TEST START DATE: 10/9/2000
 TEST START TIME: 11:48
 TEST LOCATION: RINKER RUN 2
 EMPLOYEE NAME: —
 EMPLOYEE NUMBER: —
 DEPARTMENT: —
 COMMENT FIELD 1: O2 SPAN = 25 %, SO2 SPAN = 100 PPM
 COMMENT FIELD 2: NOX SPAN = 1000 PPM, CO SPAN = 1000 PPM
 NUMERIC CODES: — — — — —

METROSONICS dl-714 SN 1554 V2.3 07/91

CURRENT DATE: 10/09/00
 CURRENT TIME: 13:20:19

TEST STARTING DATE: 10/ 9/ 0
 TEST STARTING TIME: 11:47:12

ELAPSED TIME: 0 DAYS 1:32:23
 SAMPLE RATE: 1/sec

TIME	AVG CH 1 % O2	AVG CH 2 PPM SO2	AVG CH 3 PPM NOX	AVG CH 4 PPM CO	
10/ 9/ 0					
11:47:12	13.47	1.73	212.32	347.95	
11:48:12	13.49	2.12	206.82	342.01	<<< START RUN 2
11:49:12	13.48	2.12	210.67	339.99	
11:50:12	13.53	2.11	214.52	355.58	
11:51:12	13.50	2.02	213.42	356.37	
11:52:12	13.45	2.06	207.37	347.84	
11:53:12	13.43	2.22	213.97	329.89	
11:54:12	13.48	2.35	214.52	314.97	
11:55:12	13.53	2.36	221.67	329.33	
11:56:12	13.49	2.46	220.02	331.91	
11:57:12	13.49	2.82	219.47	321.59	
11:58:12	13.48	2.83	212.87	336.06	
11:59:12	13.43	2.77	210.67	348.29	
12: 0:12	13.42	3.06	209.57	352.33	
12: 1:12	13.36	2.80	208.47	360.63	
12: 2:12	13.31	2.77	202.42	363.77	
12: 3:12	13.26	2.54	200.77	356.70	
12: 4:12	13.23	2.49	200.77	359.17	
12: 5:12	13.20	2.94	204.07	363.32	
12: 6:12	13.27	2.56	207.37	346.49	
12: 7:12	13.34	2.77	205.72	322.49	
12: 8:12	13.36	2.58	211.22	324.96	
12: 9:12	13.35	2.37	216.17	325.74	
12:10:12	13.39	2.56	230.47	315.65	

12:11:12	13.41	2.54	232.67	310.60	
12:12:12	13.43	2.40	243.12	312.96	
12:13:12	13.44	2.36	241.47	322.60	
12:14:12	13.45	2.59	249.18	321.14	
12:15:12	13.42	2.56	246.97	316.88	
12:16:12	13.42	2.43	244.22	308.69	
12:17:12	13.44	2.50	254.13	311.50	
12:18:12	13.42	2.46	260.18	304.32	
12:19:12	13.43	2.79	259.63	297.81	
12:20:12	13.44	2.71	260.73	295.23	
12:21:12	13.44	2.25	260.18	283.45	
12:22:12	13.43	2.49	256.88	285.81	
12:23:12	13.42	2.67	254.68	296.47	
12:24:12	13.37	2.41	252.48	309.37	
12:25:12	13.30	2.69	247.52	307.01	
12:26:12	13.25	2.88	255.23	312.51	
12:27:12	13.19	2.72	255.78	317.67	
12:28:12	13.17	2.53	253.58	313.07	
12:29:12	13.18	2.41	257.98	310.04	
12:30:12	13.23	2.44	271.18	305.78	
12:31:12	13.29	2.44	260.73	306.23	
12:32:12	13.33	2.35	253.58	303.65	
12:33:12	13.36	2.36	245.32	308.47	
12:34:12	13.40	2.53	252.48	306.90	
12:35:12	13.41	2.31	260.73	301.51	
12:36:12	13.41	2.48	253.58	289.18	
12:37:12	13.41	2.63	253.03	296.92	
12:38:12	13.38	2.42	233.22	305.22	
12:39:12	13.34	2.31	236.52	303.53	
12:40:12	13.34	2.40	237.07	295.34	
12:41:12	13.37	2.43	250.28	318.68	
12:42:12	13.31	2.36	247.52	321.14	
12:43:12	13.23	2.35	245.32	318.99	
12:44:12	13.19	2.26	256.33	325.18	
12:45:12	13.13	2.26	256.33	324.96	
12:46:12	13.09	2.31	254.68	337.86	
12:47:12	13.07	2.33	243.12	342.79	
12:48:12	13.06	2.19	250.28	333.26	<<< END RUN 2
12:49:12	13.10	2.25	248.63	329.11	
12:50:12	13.11	2.50	206.82	311.50	
12:51:12	14.90	1.80	14.85	101.85	
12:52:12	19.91	1.43	2.75	3.25	
12:53:12	20.60	1.19	1.65	2.36	
12:54:12	20.66	1.25	1.65	2.13	
12:55:12	20.68	1.14	1.10	2.36	<<< ZERO AIR
12:56:12	20.70	1.23	0.55	2.24	
12:57:12	20.71	1.01	0.55	2.24	
12:58:12	20.72	0.98	1.10	2.36	
12:59:12	20.73	1.11	1.10	2.36	
13: 0:12	19.95	0.96	1.10	164.78	
13: 1:12	7.34	0.93	1.10	498.04	

13: 2:12	2.80	0.73	0.55	509.59	
13: 3:12	2.49	1.13	0.55	508.92	
13: 4:12	2.44	1.01	0.55	508.36	<<< 517 PPM CO
13: 5:12	2.36	1.13	0.55	508.81	
13: 6:12	2.38	1.02	127.06	491.42	
13: 7:12	2.40	35.37	484.05	98.26	
13: 8:12	2.34	117.88	490.10	2.80	
13: 9:12	2.31	INVALID	487.90	2.36	<<< 473 PPM NOX
13:10:12	2.31	INVALID	486.25	2.13	
13:11:12	2.31	INVALID	352.04	2.13	
13:12:12	2.57	101.63	6.60	2.13	
13:13:12	2.32	68.88	2.75	2.36	
13:14:12	2.27	49.95	1.65	2.02	
13:15:12	2.26	42.18	1.65	2.02	<<< 45.49 PPM SO2
13:16:12	2.27	39.39	1.65	2.02	
13:17:12	2.23	38.51	1.65	2.24	
13:18:12	4.04	31.38	178.22	105.78	
13:19:12	11.47	19.56	254.68	306.34	

AVERAGE 13.36 2.48 236.24 321.73

CO2 = 5.18 %

O2 = 13.00 %

CEM BIAS CORRECTION

ANALYZER RESPONSE	ZERO BIAS	SPAN GAS VALUE	SPAN GAS CORRECTED ANALYZER EFFLUANT RESPONSIVE VALUE
321.73 CO	2.10	516.80	509.50 325.56
2.48 SO2	0.75	45.49	46.36 1.72
236.24 NOX	2.20	473.00	484.50 229.53

|::

Company: CSR Rinker
Source: Cement plant - Run 3

Location: Miami, FL
Date: 10/9/00

vs =	51.08	FT/SEC	As =	95.61	ft^2
Q =	293048	acfm -			not corrected
Q(std) =	190613	dscfm -			both temperature and moisture corrected
Q(moist) =	253790	dcfm -			only moisture corrected
Q(temp) =	221643	scfm -			only temperature corrected

Moisture

Vm(Std) =	46.1097867	Bws =	0.0959763	Lower Bws
Vw(Std) =	4.89528	Bws @sat =	1	Value used
Percent Moist =			9.5976347	

Emission Rates:	CO =	222.39	lb/hr	
	NOx =	360.59	lb/hr	as NO2
	SO2 =	3.54	lb/hr	
	THC =	0.00		as Propane

EQUATIONS :

As = (PI*(Stack Dia/12)^2)/4 — Round Stacks
or
As = (Stack L/12)*(Stack W/12) — Square Stacks

Md = (.44*%CO2)+(.32*%O2)+(.28*(100-(%CO2+%O2)))

Ms = (Md*(1-%Moist))+(.18*%Moist)

P(stack) = Pb+(Ps/13.6)

vs = (85.49)*(0.85)*(Sqrt.Dp)*(Sqrt[(T(s)+460)/(Ms*P(stack))])

Q = vs * As * 60

Q(std) = Q*(1-%Moist)*(528/(Ts+460))*(P(stack)/29.92)

Vm (Std) = 17.6471 * Vm * Y * ((Pb+(dH/13.6))/(Tm+460))

Vw (Std) = 0.0471 * Vlc

Bws = (Vw(Std) / (Vm(Std)+ Vw(Std))

Bws @ Sat = Vap. Pressure of H2O @ Dew Point Temp/Ps

CO (lb/hr) = ((PPM CO)*Q(std)*28.01*60)/(385*10^6)

NOx (lb/hr) = ((PPM NOx)*Q(std)*46.006*60)/(385*10^6)

SO2 (lb/hr) = ((PPM SO2)*Q(std)*64.0648*60)/(385*10^6)

THC (lb/hr) = ((PPM THC)*Q(temp)*44.0965*60)/(385*10^6)

Company: CSR Rinker
 Cement plant - Run 3

Location: Miami, FL
 Date: 10/9/00

12
 Sqrt.Dp= 0.7764
 T(s)= 243.00

Filename:
 QuickFLOW
 [Alt-C]
 to clear input
 range

Data Point	Stack Velocity Head	Stack Gas Temp.
1	0.68	243
2	0.64	243
3	0.48	243
4	0.71	243
5	0.69	243
6	0.50	243
7	0.66	243
8	0.64	243
9	0.49	243
10	0.66	243
11	0.63	243
12	0.49	243
13	0.00	0
14	0.00	0
15	0.00	0
16	0.00	0
17	0.00	0
18	0.00	0
19	0.00	0
20	0.00	0
21	0.00	0
22	0.00	0
23	0.00	0
24	0.00	0
25	0.00	0
26	0.00	0
27	0.00	0
28	0.00	0
29	0.00	0
30	0.00	0
31	0.00	0
32	0.00	0
33	0.00	0
34	0.00	0
35	0.00	0
36	0.00	0

Pb = 30.18 in Hg
 Ps = -0.68 in H2O
 %O2 = 13.27 %
 %CO2 = 5.34 %
 %Moist = 14.00 %
 Stack Dia= 132.4 in
 or
 Stack L = in
 Stack W = in
 PPM CO = 267.28 ppm
 PPM NOx = 263.85 ppm
 PPM SO2 = 1.86 ppm
 PPM THC = 0 ppm
 Vm = 47.31 ft3
 dH = 1.84 in H2O
 Tm = 90 F
 Y = 1.002
 Vlc = 104 ml

TEST START DATE: 10/9/2000
 TEST START TIME: 13:25
 TEST LOCATION: RINKER RUN 3
 EMPLOYEE NAME: ---
 EMPLOYEE NUMBER: ---
 DEPARTMENT: ---
 COMMENT FIELD 1: O2 SPAN = 25 %, SO2 SPAN = 100 PPM
 COMMENT FIELD 2: NOX SPAN = 1000 PPM, CO SPAN = 1000 PPM
 NUMERIC CODES: --- --- --- ---

METROSONICS dl-714 SN 1554 V2.3 07/91

CURRENT DATE: 10/09/00
 CURRENT TIME: 15:15:38

TEST STARTING DATE: 10/ 9/ 0
 TEST STARTING TIME: 11:47:12

ELAPSED TIME: 0 DAYS 3:25:43
 SAMPLE RATE: 1/sec

TIME	AVG CH 1 % O2	AVG CH 2 PPM SO2	AVG CH 3 PPM NOX	AVG CH 4 PPM CO	
10/ 9/ 0					
13:21:14	13.24	8.62	244.22	308.02	
13:22:14	13.32	6.49	266.78	295.34	
13:23:14	13.37	5.44	273.38	268.54	
13:24:14	13.39	4.56	272.83	264.72	
13:25:14	13.38	4.12	277.23	266.29	<<< START RUN 3
13:26:14	13.31	4.05	262.38	280.09	
13:27:14	13.30	3.79	265.68	277.85	
13:28:14	13.30	3.42	255.78	287.49	
13:29:14	13.25	3.24	253.03	294.00	
13:30:14	13.18	3.30	262.38	288.84	
13:31:14	13.15	3.15	264.58	289.18	
13:32:14	13.16	3.12	273.93	289.40	
13:33:14	13.15	3.02	265.68	283.68	
13:34:14	13.18	3.04	264.58	288.17	
13:35:14	13.23	3.01	268.98	282.45	
13:36:14	13.27	3.03	281.63	260.68	
13:37:14	13.29	2.82	287.68	261.58	
13:38:14	13.31	3.14	286.58	259.11	
13:39:14	13.36	2.89	277.78	260.80	
13:40:14	13.37	2.73	264.58	255.86	
13:41:14	13.39	2.78	264.03	264.61	
13:42:14	13.40	2.37	279.43	263.04	
13:43:14	13.40	2.58	279.98	267.86	
13:44:14	13.39	2.58	278.88	271.68	

13:45:14	13.45	2.79	275.03	263.60	
13:46:14	13.44	2.73	270.63	266.74	
13:47:14	13.41	2.79	270.08	259.67	
13:48:14	13.41	2.83	277.23	263.94	
13:49:14	13.42	2.95	263.48	277.17	
13:50:14	13.43	2.59	281.08	275.72	
13:51:14	13.39	2.78	289.33	262.82	
13:52:14	13.35	3.04	278.88	256.53	
13:53:14	13.39	2.68	271.73	268.20	
13:54:14	13.43	3.04	284.93	266.18	
13:55:14	13.42	3.00	289.33	254.29	
13:56:14	13.41	2.59	290.43	258.55	
13:57:14	13.42	3.03	281.08	258.44	
13:58:14	13.48	2.70	275.03	264.39	
13:59:14	13.46	2.91	275.03	256.98	
14: 0:14	13.47	3.09	271.73	260.24	
14: 1:14	13.47	2.70	282.73	258.10	
14: 2:14	13.46	2.82	288.78	251.71	
14: 3:14	13.48	2.71	288.78	248.46	
14: 4:14	13.43	3.11	277.78	254.85	
14: 5:14	13.41	2.74	276.13	251.26	
14: 6:14	13.41	2.90	277.23	254.40	
14: 7:14	13.40	2.72	266.78	262.48	
14: 8:14	13.39	2.56	260.73	262.70	
14: 9:14	13.38	2.82	259.63	271.12	
14:10:14	13.36	2.62	266.78	255.19	
14:11:14	13.38	2.90	271.73	257.88	
14:12:14	13.36	2.96	269.53	247.11	
14:13:14	13.38	2.63	273.93	248.91	
14:14:14	13.40	2.77	289.88	245.32	
14:15:14	13.44	3.05	282.73	240.27	
14:16:14	13.47	2.85	283.83	248.79	
14:17:14	13.46	2.78	279.98	250.59	
14:18:14	13.48	2.98	276.68	250.14	
14:19:14	13.47	2.73	275.58	254.63	
14:20:14	13.46	2.90	272.28	257.99	
14:21:14	13.48	2.80	270.08	260.24	
14:22:14	13.49	2.47	288.98	262.37	
14:23:14	13.49	2.79	273.93	252.61	
14:24:14	13.46	3.03	289.53	244.08	
14:25:14	13.46	2.95	262.38	255.30	<<< END RUN 3
14:26:14	13.49	2.77	266.23	250.81	
14:27:14	13.53	2.94	266.78	252.16	
14:28:14	13.50	2.79	260.73	263.49	
14:29:14	13.45	2.77	253.58	277.29	
14:30:14	13.69	2.81	72.06	193.27	
14:31:14	18.75	1.80	3.85	8.41	
14:32:14	20.53	1.64	2.20	2.02	
14:33:14	20.62	1.49	1.65	1.23	
14:34:14	20.64	1.28	1.65	1.35	<<< ZERO AIR
14:35:14	20.64	1.42	1.10	1.35	

14:35:14	20.64	1.14	1.10	1.57	
14:37:14	17.99	1.42	1.10	275.38	
14:38:14	4.82	1.28	1.10	504.99	
14:39:14	2.67	1.21	0.55	506.34	
14:40:14	2.53	1.31	1.10	507.35	
14:41:14	2.47	1.10	1.10	507.68	<<< 517 PPM CO
14:42:14	2.42	1.10	0.55	505.78	
14:43:14	2.56	1.22	1.10	352.10	
14:44:14	2.45	1.39	0.55	297.70	
14:45:14	2.31	1.18	1.10	298.04	<<< 309 PPM CO
14:46:14	2.36	1.42	0.55	297.59	
14:47:14	2.37	1.42	0.55	442.18	
14:48:14	2.50	1.38	0.55	828.15	
14:49:14	2.33	1.34	0.00	841.05	<<< 855 PPM CO
14:50:14	2.30	1.57	90.76	828.72	
14:51:14	2.45	51.85	482.95	201.46	
14:52:14	2.36	INVALID	489.00	2.13	
14:53:14	2.32	INVALID	486.80	1.57	<<< 473 PPM NOX
14:54:14	2.29	INVALID	485.70	1.68	
14:55:14	2.30	INVALID	665.57	1.68	
14:56:14	2.34	INVALID	952.15	1.91	
14:57:14	2.34	INVALID	950.50	1.91	<<< 941 PPM NOX
14:58:14	2.30	INVALID	948.29	1.23	
14:59:14	2.34	INVALID	650.72	1.46	
15: 0:14	2.81	117.58	7.70	1.79	
15: 1:14	2.37	93.11	2.75	1.68	
15: 2:14	2.27	69.55	1.65	1.57	
15: 3:14	2.29	59.49	0.55	1.79	
15: 4:14	2.27	54.25	0.55	1.46	
15: 5:14	2.30	50.24	0.55	1.46	
15: 6:14	2.27	48.25	0.55	1.57	
15: 7:14	2.27	47.65	0.55	1.46	
15: 8:14	2.18	47.36	0.55	1.46	<<< 45.49 PPM SO2
15: 9:14	2.26	53.65	0.55	1.57	
15:10:14	2.26	78.99	0.55	1.46	
15:11:14	2.25	93.20	0.55	1.12	
15:12:14	2.17	96.31	2.20	0.34	<<< 95.46 PPM SO2
15:13:14	0.26	93.90	8.25	0.45	
15:14:14	-0.25	82.22	8.25	0.45	

AVERAGE 13.38 2.92 274.20 263.16

CO2 = 5.34 %


O2 = 13.27 %

CEM BIAS CORRECTION

ANALYZER RESPONSE		ZERO BIAS	SPAN GAS VALUE	SPAN GAS CORRECTED ANALYZER EFFLUANT RESPONSIVE VALUE	
263.16	CO	1.10	516.80	507.80	267.28
2.92	SO2	1.03	45.49	47.11	1.86
274.20	NOX	1.95	473.00	490.00	263.85

FIELD AND LABORATORY DATA SHEETS



ch1 02
 ch2 802
 ch3 NOY
 ch4 CO


Date: 10/9/00
 Plant: Rin Kor
 Location: Miami Florida
 Source: Cement Plant

RUN NO.	START TIME	END TIME	OST CO2 %	OST O2 %	CO ppm	SO2 ppm	NOx ppm	THC ppm	KA O2 %
1	10:13	11:13	5.93	13.77	302.36	1.83	249.24	/	13.27
	199825 DSCFM	232355 SCFM			ppm corr 305.01	ppm corr 0.87	ppm corr 245.99	/	-
	222762	235770			LB/HR 266.05	LB/HR 1.74	LB/HR 352.43	/	-
2	11:48	12:48	5.13	13.0	321.73	2.48	236.24	/	13.36
	207015 DSCFM	235244 SCFM			corr ppm 335.56	corr ppm 1.72	corr ppm 229.53	/	-
					LB/HR 290.73	LB/HR 3.55	LB/HR 340.68	/	-
3	13:25	14:25	5.34	13.27	263.16	2.92	274.2	/	13.58
	202601 DSCFM	235583 SCFM			ppm corr 267.28	ppm corr 1.86	ppm corr 263.85	/	-
					LB/HR 236.38	LB/HR 3.76	LB/HR 383.27	/	-

Rinkor Cement PLANT
10/9/00
System Calibration Bias And Drift Data

Date of Final Value	Time of Final Value		Cal. Gas Value (ppm)	INITIAL VALUE	FINAL VALUES	Absolute Difference (ppm)	Difference (percent of span)
				System Calibration Response (ppm)	System Calibration Response (ppm)		

NOx Analyser

		Zero gas	0	1.1	}		
		Upscale gas	473	477	}		
	11:19	Zero gas	0	{	2.7		
	11:30	Upscale gas	473		478		
	12:54	Zero gas	0	{	1.7		
	13:08	Upscale gas	473		491		
	14:33	Zero gas	0	{	2.2		
	14:52	Upscale gas	473		489		

SO2 Analyser

		Zero gas	0	1.25	}		
		Upscale gas	45.49	44.98	}		
	11:19	Zero gas	0	{	0.67		
	11:34	Upscale gas	45.49		47.09		
	12:55	Zero gas	0	{	0.83		
	13:15	Upscale gas	45.49		45.62		
	14:33	Zero gas	0	{	1.23		
	15:06	Upscale gas	45.49		48.6		

CO Analyser

		Zero gas	0	5.0	}		
		Upscale gas	516.8	509	}		
	11:19	Zero gas	0	{	3.1		
	11:24	Upscale gas	516.8		510		
	12:54	Zero gas	0	{	1.1		
	13:03	Upscale gas	516.8		509		
	14:35	Zero gas	0	{	1.1		
	14:39	Upscale gas	516.8		506.6		

THC Analyser

		Zero gas					
		Upscale gas					
		Zero gas					
		Upscale gas					
		Zero gas					
		Upscale gas					
		Zero gas					
		Upscale gas					

PLANT: R. H. K. Cement Plant

EPA METHOD 3

ANALYSIS TOLERANCE

DATE: 10/9/00

ORSAT ANALYSIS
B. B. ...
...

CO₂ = 0.9 %
O₂ = 0.7 %
CO = 1.2 %

SOURCE: Cement Kiln

RUN NO.	ANALYSIS NO.	OXYGEN PERCENT	OXYGEN AVERAGE	CARBON DIOXIDE PERCENT	CARBON DIOXIDE AVERAGE
1	1	13.8		6.0	
	2	13.7		5.9	
	3	13.8	13.77	5.9	5.93
2	1	12.9		5.0	
	2	13.1		5.2	
	3	13.0	13.0	5.2	5.13
3	1	13.3		5.3	
	2	13.3		5.3	
	3	13.2	13.27	5.4	5.34
4	1				
	2				
	3				
5	1				
	2				
	3				
6	1				
	2				
	3				
7	1				
	2				
	3				
8	1				
	2				
	3				
9	1				
	2				
	3				
10	1				
	2				
	3				

KOUGLER & ASSOCIATES
CEM RESPONSE TIME DETERMINATION

Date: 10/9/00

Location: A. Ont, Pa.

Source: Rinker, Cement Plant

Pollutant: SO₂

Monitor: SO₂, W.R. 721AT

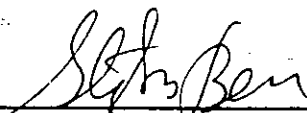
Serial Number: 92-721AT2-7124-1

Low Range Concentration: 0 ppm

Mid Range Concentration: 45.49 ppm

High Range Concentration: 96 ppm

TEST RUN	UPSCALE TEST		DOWNSCALE TEST	
	LOW TO MID RANGE (minutes)	MID TO HIGH RANGE (minutes)	HIGH TO MID RANGE (minutes)	MID TO LOW RANGE (minutes)
1	1.95			1.86
2	1.99			1.92
3	1.97			1.89
AVERAGE	1.97			1.89
AVERAGE				

Signature: 

KOGLER & ASSOCIATES
CEM RESPONSE TIME DETERMINATION

Date: 10/9/00

Location: MIAMI FL

Source: Rinker, Cement PLANT

Pollutant: NOX

Monitor: NOX, TECO 105

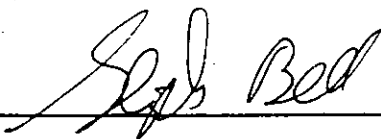
Serial Number: 105-33475-245

Low Range Concentration: 0 ppm

Mid Range Concentration: 473 ppm

High Range Concentration: 941 ppm

TEST RUN	UPSCALE TEST		DOWNSCALE TEST	
	LOW TO MID RANGE (minutes)	MID TO HIGH RANGE (minutes)	HIGH TO MID RANGE (minutes)	MID TO LOW RANGE (minutes)
1	0.90			0.91
2	0.85			0.88
3	0.91			0.89
AVERAGE	0.88			0.89
AVERAGE				

Signature: 

KOUGLER & ASSOCIATES
CEM RESPONSE TIME DETERMINATION

Date: 10/9/00

Location: Miami

Source: Rinker, Cement Plant

Pollutant: CO

Monitor: CO, TECO 484

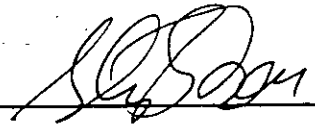
Serial Number: 484 31635-241

Low Range Concentration: 0 ppm

Mid Range Concentration: 516.8 ppm

High Range Concentration: 855 ppm

TEST RUN	UPSCALE TEST		DOWNSCALE TEST	
	LOW TO MID RANGE (minutes)	MID TO HIGH RANGE (minutes)	HIGH TO MID RANGE (minutes)	MID TO LOW RANGE (minutes)
1	1.8			1.6
2	1.7			1.6
3	1.7			1.65
AVERAGE	1.73			1.61
AVERAGE				

Signature: 

K.A.CEM

SOURCE: <i>2.2 kv Cement plant</i>	DATE: <i>10/9/00</i>
MONITOR: <i>NOX, 105</i>	LOCATION: <i>M. And FL.</i>
SERIAL NUMBER: <i>105-33495-245</i>	SPAN: <i>1000 ppm</i>

RUN NUMBER	CALIBRATION VALUE	MONITOR RESPONSE	DIFFERENCE		
			Zero/Low	Mid	High
1 - Zero	0	0.5	0.5		
2 - Mid	473	470.3		-2.7	
3 - High	941	932			-9
4 - Mid	473	487.9		14.9	
5 - Zero	0	1.10	1.10		
6 - High	941	—			—
7 - Zero	0	1.65	1.65		
8 - Mid	473	486.8		13.8	
9 - High	941	954			13
MEAN DIFFERENCE -			1.08	8.66	2
CALIBRATION ERROR -			0.12 %	0.86 %	0.40 %

Calibration Error Determination



K/A CEM.

SOURCE: <i>Rinker, Cement Plant</i>	DATE: <i>10/9/00</i>
MONITOR: <i>SO₂, W.R. 721AT</i>	LOCATION: <i>Miami FL</i>
SERIAL NUMBER: <i>92-721A72-7924-1</i>	SPAN: <i>100ppm</i>

RUN NUMBER	CALIBRATION VALUE	MONITOR RESPONSE	DIFFERENCE		
			Zero/Low	Mid	High
1 - Zero	0	1.8	1.8		
2 - Mid	45.49	44.35		-1.14	
3 - High	95.46	95.2			0.2
4 - Mid	45.49	42.18		-3.31	
5 - Zero	0	1.14	1.14		
6 - High	95.46	—			
7 - Zero	0	1.28	1.28		
8 - Mid	45.49	47.36		+1.87	
9 - High	95.46	96.39			0.93
MEAN DIFFERENCE =			1.41	-0.86	0.56
CALIBRATION ERROR =			6.41 %	-0.86 %	0.56 %

Calibration Error Determination



SOURCE: Rinkor Demolition Plant	DATE: 10/9/80
MONITOR: CO, TECO 484	LOCATION: Miami FL
SERIAL NUMBER: 484-31635-241	SPAN: 1000ppm

RUN NUMBER	CALIBRATION VALUE	MONITOR RESPONSE	DIFFERENCE		
			Zero/Low	Mid	High
1 - Zero	0	6.1	6.1		
2 - Mid	516.8	521.3		4.5	
3 - High	855	857			2.0
4 - Mid	516.8	508.36		-8.44	
5 - Zero	0	2.36	2.36		
6 - High	855	840.4			-14.6
7 - Zero	0	1.35	1.35		
8 - Mid	516.8	507.68		-9.12	
9 - High	855	841.05			-13.95
MEAN DIFFERENCE -			3.27	-4.35	10.18
CALIBRATION ERROR -			0.33 %	0.43 %	1.02 %

Calibration Error Determination



PLANT INFORMATION

P.2/2

10/09/00

Clinker - 2,480.60
(103.9 tons P/hour)

Coal used - 311.50 (13.0 tph)

Kiln Feed used - 4,134.40 (172.3 tph)

Total Clinker	+ TPH
" Coal used	
" Feed To Kiln	

CERTIFICATE OF ANALYSIS





1250 W. Washington
West Chicago, IL 60185
Phone: (630) 231-9260
FAX: (630) 231-4071

Certificate of Analysis: E.P.A. Protocol Gas Mixture

Cylinder No.:	<u>CC91937</u>	Order No.:	<u>GM 2000361</u>
Cylinder Pressure:	<u>2000 psig</u>	Expiration Date:	<u>5/17/02</u>
Certification Date:	<u>5/17/00</u>	Laboratory:	<u>W. Chicago</u>

Reference Standard Information:

<u>Type</u>	<u>Component</u>	<u>Cyl. Number</u>	<u>Concentration</u>
SRM 1694a	Sulfur Dioxide	CAL-010631	97.6 ppm

Instrumentation:

<u>Instrument/Model/Serial No.</u>	<u>Analytical Principle</u>
Nicolet/8220/AAB9400246	FTIR

Analytical Methodology does not require correction for analytical interferences.

Analytical Results:

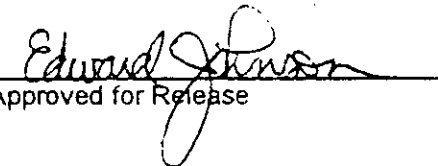
<u>1st Component:</u>		<u>Sulfur Dioxide:</u>					
1st Analysis Date: <u>5/10/00</u>							
R	<u>96.629</u>	S	<u>94.502</u>	Z	<u>-0.003</u>	Conc	<u>95.439 ppm</u>
S	<u>94.520</u>	Z	<u>0.012</u>	R	<u>96.583</u>	Conc	<u>95.457 ppm</u>
Z	<u>0.014</u>	R	<u>96.713</u>	S	<u>94.308</u>	Conc	<u>95.243 ppm</u>
						AVG:	<u>95.380 ppm</u>
2nd Analysis Date: <u>5/17/00</u>							
R	<u>95.881</u>	S	<u>93.857</u>	Z	<u>-0.038</u>	Conc	<u>95.472 ppm</u>
S	<u>93.979</u>	Z	<u>-0.048</u>	R	<u>96.027</u>	Conc	<u>95.586 ppm</u>
Z	<u>-0.036</u>	R	<u>95.972</u>	S	<u>93.964</u>	Conc	<u>95.571 ppm</u>
						AVG:	<u>95.543 ppm</u>

Certified Concentrations:

<u>Component</u>	<u>Concentration</u>	<u>Accuracy</u>	<u>Procedure</u>
Sulfur Dioxide	95.46 ppm	+/- 1%	G1
Nitrogen	Balance		

Certification performed in accordance with "EPA Traceability Protocol (Sept. 1997)" using the assay procedures listed.

Do not use cylinder below 150 psig.


Approved for Release



1250 W. Washington
West Chicago, IL 60185
Phone: (630) 231-9260
FAX: (630) 231-4071

Certificate of Analysis: E.P.A. Protocol Gas Mixture

Cylinder No :	<u>CC108987</u>	Order No.	<u>GM 2000360</u>
Cylinder Pressure:	<u>2000 psig</u>	Expiration Date:	<u>5/17/02</u>
Certification Date	<u>5/17/00</u>	Laboratory:	<u>W. Chicago</u>

Reference Standard Information:

<u>Type</u>	<u>Component</u>	<u>Cyl. Number</u>	<u>Concentration</u>
SRM 1693a	Sulfur Dioxide	CAL-010573	49.9 ppm

Instrumentation:

<u>Instrument/Model/Serial No.</u>	<u>Analytical Principle</u>
Nicolet/8220/AAB9400246	FTIR

Analytical Methodology does not require correction for analytical interferences.

Analytical Results:

1st Component: Sulfur Dioxide

1st Analysis Date: <u>5/10/00</u>					
R	<u>50.317</u>	S	<u>45.851</u>	Z	<u>-0.054</u>
S	<u>45.844</u>	Z	<u>-0.050</u>	R	<u>50.293</u>
Z	<u>-0.050</u>	R	<u>50.321</u>	S	<u>45.932</u>
				Conc	<u>45.482 ppm</u>
				Conc	<u>45.475 ppm</u>
				Conc	<u>45.562 ppm</u>
				AVG:	<u>45.506 ppm</u>

2nd Analysis Date: <u>5/17/00</u>					
R	<u>50.001</u>	S	<u>45.629</u>	Z	<u>-0.028</u>
S	<u>45.547</u>	Z	<u>-0.011</u>	R	<u>50.022</u>
Z	<u>-0.017</u>	R	<u>50.036</u>	S	<u>45.567</u>
				Conc	<u>45.521 ppm</u>
				Conc	<u>45.440 ppm</u>
				Conc	<u>45.460 ppm</u>
				AVG:	<u>45.474 ppm</u>

Certified Concentrations:

<u>Component</u>	<u>Concentration</u>	<u>Accuracy</u>	<u>Procedure</u>
Sulfur Dioxide	45.49 ppm	+/- 1%	G1
Nitrogen	Balance		

Certification performed in accordance with "EPA Traceability Protocol (Sept. 1997)" using the assay procedures listed.

Do not use cylinder below 150 psig.

Edward Johnson

 Approved for Release

For Technical Information Call
1-800-752-1597



CERTIFICATE OF ANALYSIS: EPA PROTOCOL GAS STANDARD

PERFORMED ACCORDING TO EPA TRACEABILITY PROTOCOL FOR ASSAY AND CERTIFICATION OF GASEOUS CALIBRATION STANDARDS (PROCEDURE #G1)

Order No: 854-055359-1

Batch No: 59019

Cylinder Number: SG-9169105

Bar Code No: DNK967

Cylinder pressure*: 2000

Certification Date: 11-8-99

Expiration Date: 11/8/01

CERTIFIED CONCENTRATION		REFERENCE STANDARDS			ANALYTICAL INSTRUMENTATION			
Component	Certified Concentration	Cylinder Number	Standard Type	Standard Concentration	Instrument Make/Model	Serial Number	Last Calibration	Measurement Principle
Carbonic Oxide	473 ± 4 ppm	CLM-09974	SRM-1888b	481.6 ppm	Nicolet 550	ACN-9402192	10-18-99	FTIR
Sulfur Dioxide	652 ± 5 ppm	SX-37584	NTRM-81675	1478 ppm	Nicolet 550	ACN-9402192	10-18-99	FTIR

Oxygen Balance Gas

Oxygen (Reference value only): <2 ppm

*STANDARD SHOULD NOT BE USED BELOW 150 PSIG

Notes:

John J Hudy

Approved By:
John Peters

For Technical Information Call
1-800-752-1597



Air Products and Chemicals, Inc. • 12722 S. Wentworth Avenue, Chicago, IL 60628

ISO CERTIFICATION: 9002

CERTIFICATE OF ANALYSIS: EPA PROTOCOL GAS STANDARD

PERFORMED ACCORDING TO EPA TRACEABILITY PROTOCOL FOR ASSAY AND CERTIFICATION OF GASEOUS CALIBRATION STANDARDS (PROCEDURE #G1)

Customer: AIR PRODUCTS & CHEMICALS, INC.
5837 W. 5TH STREET
JACKSONVILLE

Order No: 854-054693-01
Batch No: 861-56854
PO:
FL 32254-1509 **Release:**

Cylinder No: SG9148860BAL
Bar Code No: DRD479
Cylinder Pressure*: 2000 psig
Certification Date: 05/10/1999
Expiration Date: 05/10/2001

CERTIFIED CONCENTRATION		REFERENCE STANDARDS			ANALYTICAL INSTRUMENTATION			
Component	Certified Concentration	Cylinder Number	Standard Type	Standard Concentration	Instrument Make/Model	Serial Number	Last Calibration	Measurement Principal
NITRIC OXIDE	941±4 PPM	SG9150562BAL	NTRM 81687X	844.0 PPM	THERMO ENVIRO	52829293	04/21/99	CHEMILUMINESCENCE
SULFUR DIOXIDE	1120±21 PPM	SG9128413BAL	NTRM 81664	2502 PPM	BOVAR 721M PHO	8327-3	04/12/99	NON DISPERSIVE ULTRAVIOLET

NO2 (Reference Value Only): 1.00 PPM

NITROGEN Balance Gas

* STANDARD SHOULD NOT BE USED BELOW 150 PSIG

Analyst:

James Laab

Approved By:

Richard Fry

5480 Hamilton Blvd.
Theodore, AL 36582

P.O. Box 190969
Mobile, AL 36619

Phone: (334) 653-2500
FAX: (334) 653-2530

Certificate of Analysis: E.P.A. Protocol Gas Mixture

Cylinder No :	<u>CC19573</u>	Order No.	<u>400220</u>
Cylinder Pressure:	<u>2000 PSIG</u>	Expiration Date:	<u>6/30/03</u>
Certification Date	<u>6/30/00</u>	Laboratory:	<u>ASG-MOBILE</u>

Reference Standard Information:

<u>Type</u>	<u>Component</u>	<u>Cyl. Number</u>	<u>Concentration</u>
NTRM81681	CARBON MONOXIDE	CC67933	1005PPM

Instrumentation:

<u>Instrument/Model/Serial No.</u>	<u>Analytical Principle</u>
SIEMENS ULTRAMAT 5E J9-661	NDIR

Analytical Methodology does not require correction for analytical interferences.

Certified Concentrations:

<u>Component</u>	<u>Concentration</u>	<u>Accuracy</u>	<u>Procedure</u>
CARBON MONOXIDE	516.8 PPM	+/-1%	G1
NITROGEN	Balance		

Analytical Results:

1st Component:

CARBON MONOXIDE

1st Analysis Date: 6/23/00

R	<u>1005</u>	S	<u>516.0</u>	Z	<u>0.000</u>	Conc	<u>516.0</u>
S	<u>517.0</u>	Z	<u>0.000</u>	R	<u>1005</u>	Conc	<u>517.0</u>
Z	<u>0.000</u>	R	<u>1005</u>	S	<u>517.0</u>	Conc	<u>517.0</u>
						AVG:	<u>516.7</u>

2nd Analysis Date: 6/30/00

R	<u>1004</u>	S	<u>516.0</u>	Z	<u>0.000</u>	Conc	<u>516.5</u>
S	<u>517.0</u>	Z	<u>0.000</u>	R	<u>1005</u>	Conc	<u>517.0</u>
Z	<u>0.000</u>	R	<u>1005</u>	S	<u>517.0</u>	Conc	<u>517.0</u>
						AVG:	<u>516.8</u>

Certification performed in accordance with "EPA Traceability Protocol (Sept. 1997)" using the assay procedures listed.

Do not use cylinder below 150 psig.

Bridget H. Richardson
Approved for Release

Airgas

Specialty Gases

5480 Hamilton Blvd.
Theodore, AL 36582

P.O. Box 190969
Mobile, AL 36619

Phone: (334) 653-2500
FAX: (334) 653-2530

Certificate of Analysis: E.P.A. Protocol Gas Mixture

Cylinder No :	<u>CC19513</u>	Order No.	<u>400220</u>
Cylinder Pressure:	<u>2000 PSIG</u>	Expiration Date:	<u>6/30/03</u>
Certification Date	<u>6/30/00</u>	Laboratory:	<u>ASG-MOBILE</u>

Reference Standard Information:

<u>Type</u>	<u>Component</u>	<u>Cyl. Number</u>	<u>Concentration</u>
NTRM81681	CARBON MONOXIDE	CC67933	1005PPM

Instrumentation:

<u>Instrument/Model/Serial No.</u>	<u>Analytical Principle</u>
SIEMENS ULTRAMAT 5E J9-661	NDIR

Analytical Methodology does not require correction for analytical interferences.

Certified Concentrations:

<u>Component</u>	<u>Concentration</u>	<u>Accuracy</u>	<u>Procedure</u>
CARBON MONOXIDE	309.1 PPM	+/-1%	G1
NITROGEN	Balance		

Analytical Results:

1st Component:

CARBON MONOXIDE

1st Analysis Date:	<u>6/23/00</u>						
R	<u>1005</u>	S	<u>309.0</u>	Z	<u>0.000</u>	Conc	<u>309.0</u>
S	<u>309.0</u>	Z	<u>0.000</u>	R	<u>1005</u>	Conc	<u>309.0</u>
Z	<u>0.000</u>	R	<u>1005</u>	S	<u>309.0</u>	Conc	<u>309.0</u>
						AVG:	<u>309.0</u>

2nd Analysis Date:	<u>6/30/00</u>						
R	<u>1004</u>	S	<u>309.0</u>	Z	<u>0.000</u>	Conc	<u>309.3</u>
S	<u>309.0</u>	Z	<u>0.000</u>	R	<u>1005</u>	Conc	<u>309.0</u>
Z	<u>0.000</u>	R	<u>1005</u>	S	<u>309.0</u>	Conc	<u>309.0</u>
						AVG:	<u>309.1</u>

Certification performed in accordance with "EPA Traceability Protocol (Sept. 1997)" using the assay procedures listed.

Do not use cylinder below 150 psig.

Bridget H. Richardson
Approved for Release

Airgas

Specialty Gases

5480 Hamilton Blvd.
Theodore, AL 36582

P.O. Box 190969
Mobile, AL 36619

Phone: (334) 653-2500
FAX: (334) 653-2530

Certificate of Analysis: E.P.A. Protocol Gas Mixture

Cylinder No :	<u>CC19585</u>	Order No.	<u>400220</u>
Cylinder Pressure:	<u>2000 PSIG</u>	Expiration Date:	<u>6/30/03</u>
Certification Date	<u>6/30/00</u>	Laboratory:	<u>ASG-MOBILE</u>

Reference Standard Information:

Type	Component	Cyl. Number	Concentration
NTRM81681	CARBON MONOXIDE	CC67933	1005PPM

Instrumentation:

Instrument/Model/Serial No.	Analytical Principle
SIEMENS ULTRAMAT 5E J9-661	NDIR

Analytical Methodology does not require correction for analytical interferences.

Certified Concentrations:

Component	Concentration	Accuracy	Procedure
CARBON MONOXIDE	855.2 PPM	+/-1%	G1
NITROGEN	Balance		

Analytical Results:

1st Component:

CARBON MONOXIDE

1st Analysis Date: <u>6/23/00</u>							
R	<u>1005</u>	S	<u>855.0</u>	Z	<u>0.000</u>	Conc	<u>855.0</u>
S	<u>855.0</u>	Z	<u>0.000</u>	R	<u>1005</u>	Conc	<u>855.0</u>
Z	<u>0.000</u>	R	<u>1005</u>	S	<u>855.0</u>	Conc	<u>855.0</u>
						AVG:	<u>855.0</u>

2nd Analysis Date: <u>6/30/00</u>							
R	<u>1004</u>	S	<u>855.0</u>	Z	<u>0.000</u>	Conc	<u>855.9</u>
S	<u>855.0</u>	Z	<u>0.000</u>	R	<u>1005</u>	Conc	<u>855.0</u>
Z	<u>0.000</u>	R	<u>1005</u>	S	<u>855.0</u>	Conc	<u>855.0</u>
						AVG:	<u>855.3</u>

Certification performed in accordance with "EPA Traceability Protocol (Sept. 1997)" using the assay procedures listed.

Do not use cylinder below 150 psig.


Approved for Release

PROJECT PARTICIPANTS



PROJECT PARTICIPANTS

John B. Koogler, Ph.D., P.E.

Project Advisor

Stephen S. Bell

Field Test Crew

Glen A. Haven

Field Test Crew



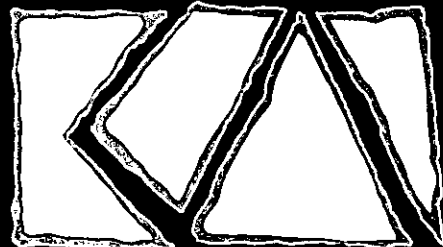
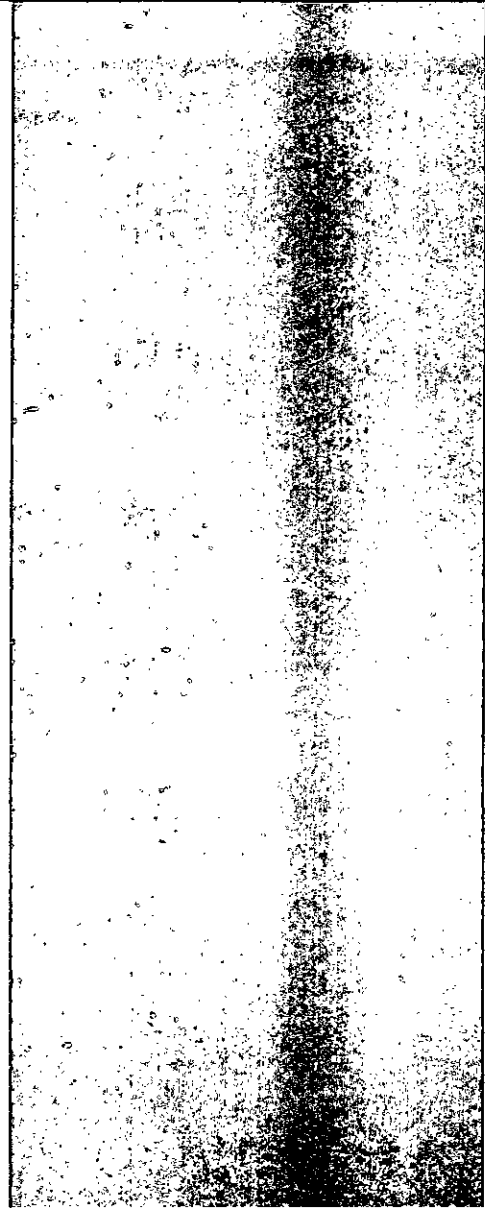
PARTICULATE MATTER EMISSION
MEASUREMENTS AND
VISIBLE EMISSIONS OBSERVATIONS

CEMENT KILN/RAW MILL/CLINKER COOLER

CSR RINKER MATERIALS CORPORATION
MIAMI, FLORIDA

AIRS I.D. NO. 0250014
PERMIT NO. 0250014-002-AC

SEPTEMBER 29, 2000



KOOGLER & ASSOCIATES

ENVIRONMENTAL SERVICES

4014 NW THIRTEENTH STREET
GAINESVILLE, FLORIDA 32609
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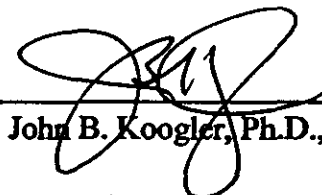
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SEPTEMBER 29, 2000

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GAINESVILLE, FLORIDA 32609
(352) 377-5822



To the best of my knowledge, all applicable field and analytical procedures comply with the Florida Department of Environmental Protection requirements and all test data and plant operating data are true and correct.



John B. Koogler, Ph.D., P.E.

State of Florida
Registration No. 12925

12/1/00

Date



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APPENDIX

1.0 INTRODUCTION

CSR Rinker Materials Corporation owns and operates a preheater/precalciner Portland cement plant located at 1200 N.W. 137th Avenue, Miami, Dade County, Florida. On September 29, 2000, Koogler & Associates Environmental Services of Gainesville, Florida, conducted particulate matter (PM/PM10) emission measurements and visible emissions observations on the kiln/raw mill/cooler in accordance with EPA Methods 5 and 9 (40 CFR 60, Appendix A). The purpose of the testing was to satisfy the emission limiting requirements of Permit No. 0250014-005-AC.

Prior to the test date, the Metropolitan Dade Environmental Resources Management (DERM) was notified of the test schedule and testing methods.

During the test period, the kiln was operating at an average preheater feed rate of 200.6 tons per hour. The PM/PM10 stack gas concentration averaged 0.0012 grains per dry standard cubic foot. The corresponding PM/PM10 emission rate averaged 2.03 pounds per hour. The permit limits the preheater feed rate to 220 tons per hour and the emission rate of PM/PM10 to 44 pounds per hour; or to 0.2 pounds per ton of preheater feed.

Visible emissions observations were conducted for a 3-hour period. During the observation periods, no visible emissions were observed. The permit limits the opacity of emissions from the kiln/raw mill/cooler to 10 percent.

Based upon the data presented herein, it can be concluded that during the period of testing on September 29, 2000, the kiln/raw mill/cooler were operating in compliance with the PM/PM10 emissions limiting standard and the visible emissions standard set forth in Permit No. 0250014-002-AC.

2.0 LOCATION OF SAMPLING PORTS

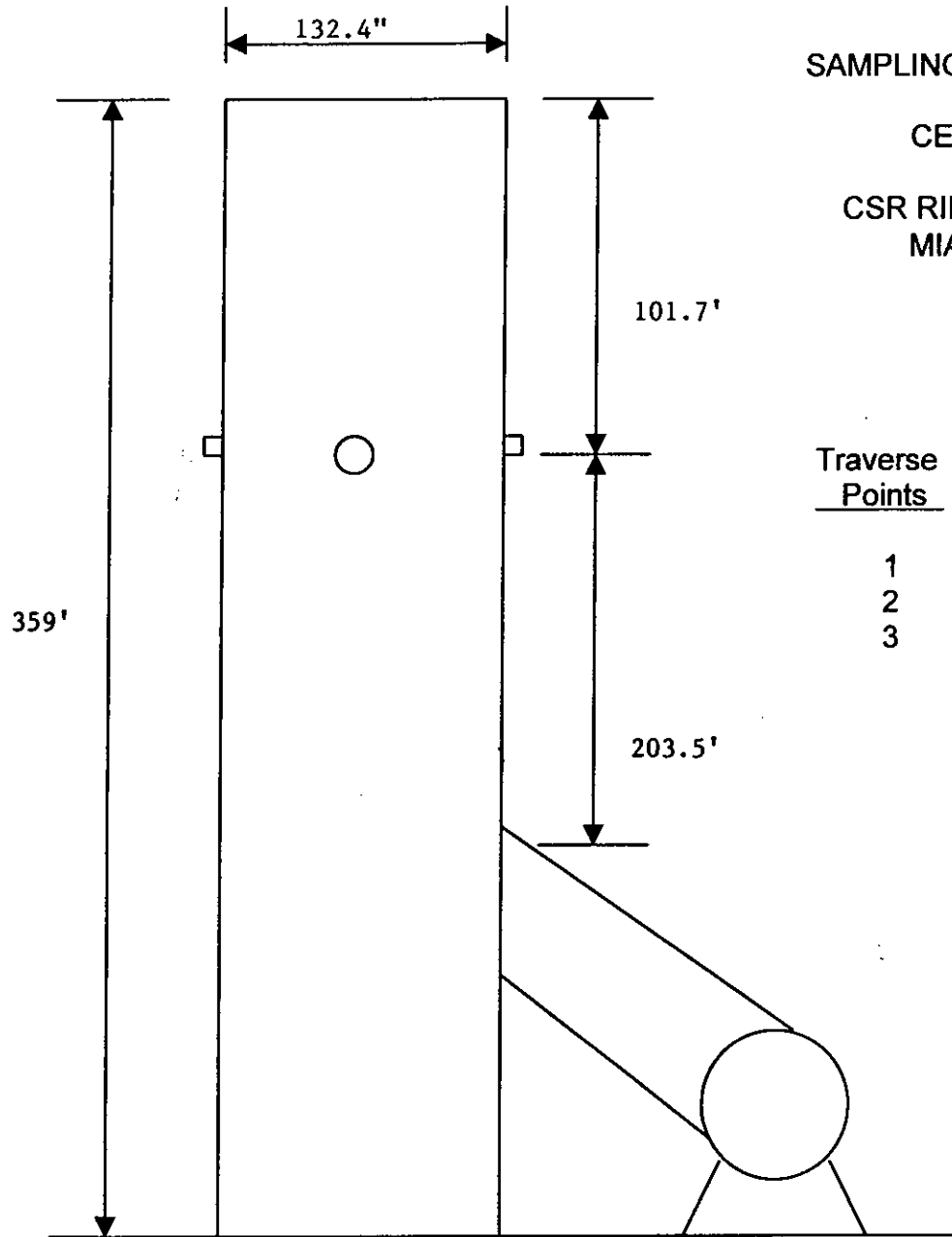
The locations of the sampling points are shown in Figure 1. Stack gas flow rate measurements and sample collection for PM/PM10 emission measurements were made through four sampling ports located 90 degrees to one another in the 136.5-inch diameter stack. The ports are located 203.5 feet (18.5 diameters) above the point where the stack gas enters the stack and 101.7 feet (9.3 diameters) below the top of the stack. A total of 12 sampling points were used for the velocity and sampling traverses. The sampling points were located in accordance with criteria established by EPA Test Method 1 (40 CFR 60, Appendix A).

FIGURE 1

SAMPLING POINT LOCATIONS

CEMENT PLANT

**CSR RINKER MATERIALS
MIAMI, FLORIDA**



<u>Traverse Points</u>	<u>Distance from Inside Stack Wall</u>
1	6.01
2	19.9
3	40.4

3.0 FIELD AND ANALYTICAL PROCEDURES

PM/PM10 emission measurements were made using EPA Method 5 as adopted by FDEP in Rule 62-297.401(5), F.A.C. All particulate matter collected by the test method was assumed to be PM10 particles. The heated filter holder was separated from the impingers with a flexible sample line as provided for in Rule 62.297.330(5), F.A.C. The sampling point locations for the EPA Method 5 test were established in accordance with EPA Method 1.

Stack gas velocity measurements and stack gas moisture measurements were made in conjunction with the EPA Method 5 tests in accordance with EPA Methods 2 and 4. Opacity observations were made in accordance with EPA Method 9. All EPA test methods are described in 40 CFR 60, Appendix A and have been adopted by reference by FDEP by Rule 62-297.401, F.A.C.

A schematic diagram of the sampling train used for the particulate matter emission measurement is shown in Figure 2.

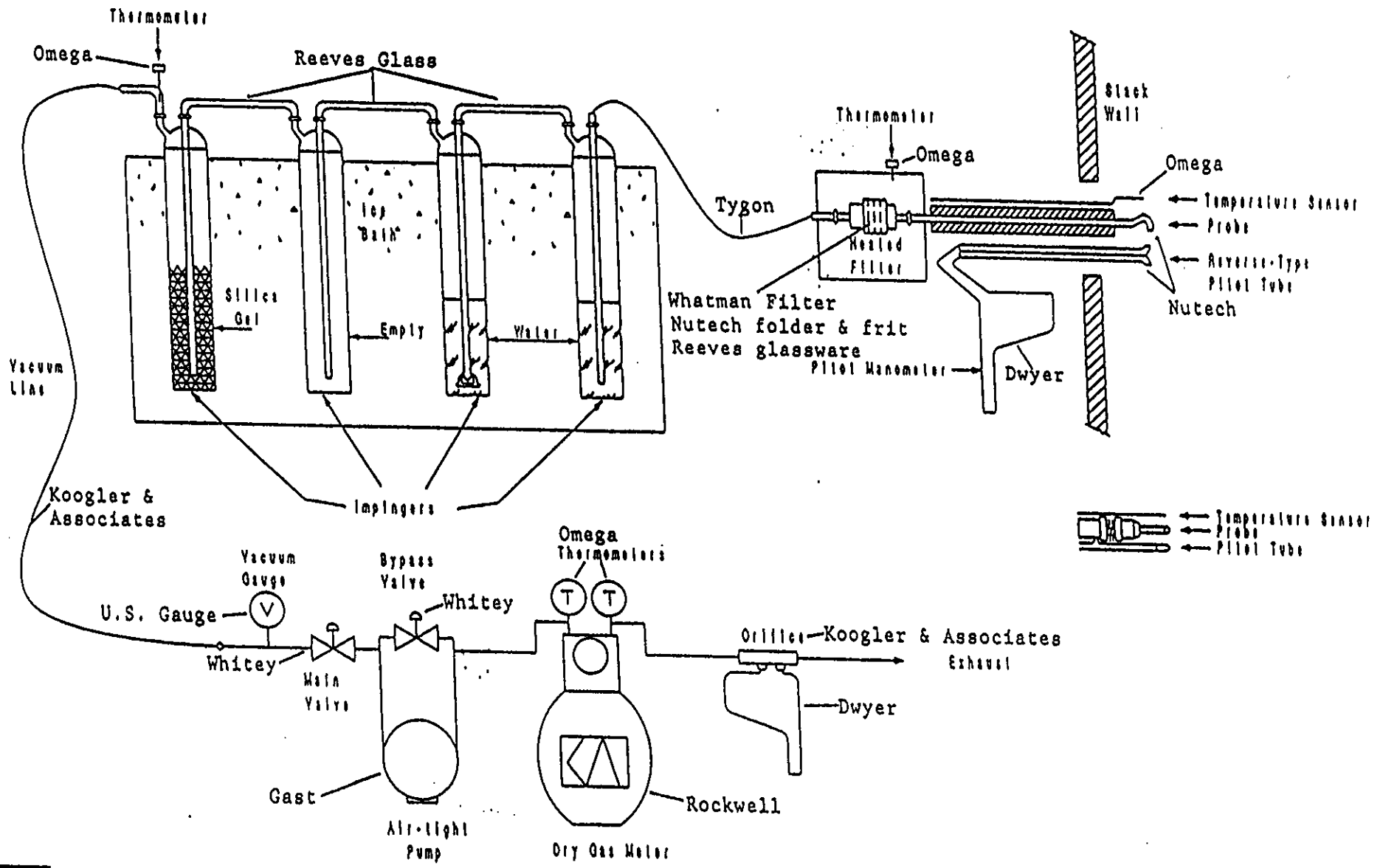


FIGURE 2
EPA METHOD 5 PARTICULATE MATTER SAMPLING TRAIN

4.0 SUMMARY OF RESULTS

Results of the particulate matter emission measurements conducted on September 29, 2000, are summarized in Table 1. The PM/PM10 stack gas concentrations ranged from 0.0008 to 0.0020 grains per dry standard cubic foot and averaged 0.0012 grains per dry standard cubic foot. The corresponding PM/PM10 emission rate averaged 2.03 pounds per hour. The stack gas flow averaged 202,343 dscfm at a temperature of 291°F and a stack gas moisture of 12.1 percent.

Visible emissions observations were conducted for a 3-hour period. During the observation period, no visible emissions were observed. The permit limits the opacity of emissions from the kiln/raw mill/cooler to 10 percent.

Based upon the data presented herein, it can be concluded that during the period of testing on September 29, 2000, the kiln/raw mill/cooler were operating in compliance with the PM/PM10 emission limiting standard and the visible emissions standard set forth in Permit No. 0250014-002-AC.

Calculations, field and laboratory data sheets, plant information, equipment calibrations and a list of project participants are included in the Appendix of this report.

TABLE 1

SUMMARY OF SOURCE EMISSION TEST DATA

RINKER / MIAMI, FL.
 CEMENT KILN
 SEPT 29, 2000

Run No.	Process Weight Rate (Tons/hr)	Stack Gas Flow Rate (SCFMD)	Stack Gas Temperature (F)	Stack Gas Moisture (%)	Particulate Matter	
					Conc. (gr/dscf)	Emission Rate (Lbs/Hr)
1	200.6	188,560	249	14.7	0.0020	3.16
2	200.6	191,866	249	13.4	0.0008	1.30
3	200.6	226,605	376	8.2	0.0008	1.63
Average	200.6	202,343	291	12.1	0.0012	2.03

Allowable Particulate Matter Emission Rate = lbs/Hr

APPENDIX

**CALCULATIONS
FIELD AND LABORATORY DATA SHEETS
PLANT INFORMATION
EQUIPMENT CALIBRATIONS
PROJECT PARTICIPANTS**

CALCULATIONS

GENERAL DATA

DATA FILE NAME: PART9-29

Company : RINKER / MIAMI, FL. *****
 Source/Unit : CEMENT KILN 01:15 PM
 Date : SEPT 29, 2000 Cp : 0.840
 Stack dia. : 132.40 inch OR : Duct Length : 0.00 inch
 Oxygen Corr.: 0.0 percent Duct Width : 0.00 inch
 CO2 Corr. : 0.0 percent Std. Temp. : 68 F

FUEL ANALYSIS DATA, (By F Factor or Fuel Use)

F Factor = F, Fuel Use = U F Process Wt.

Hydrogen, wt% : 0.00 Run 1 : 200.6 Tons/hr
 Carbon, wt% : 0.00 Run 2 : 200.6
 Sulfur, wt% : 0.00 Run 3 : 200.6
 Nitrogen, wt% : 0.00
 Oxygen, wt% : 0.00
 Btu/lb : 0

Type of Flow Meter : (1=Meter Box 2=Mass Flow Meter) 1

F-Factor : dscf/MMBtu;

FIELD DATA ----- METHOD 5 RUN RUN RUN
 1 2 3

Meter Temp., Tm (F)	85	92	92
Stack Temp., Ts (F)	249	249	376
Sq.Rt. dP	0.80	0.80	0.98
dH (in. H2O)	1.54	1.52	2.01
Meter Vol., Vm (ft3)	44.500	44.670	51.523
Meter Y	1.000	1.000	1.000
Bar. Press., Pb (in.Hg.)	30.03	30.03	30.03
Vol. H2O, Vlc (ml)	159	142	94
Static Press., Ps (in.H2O)	-0.90	-0.90	-0.90
Test Time (min.)	60.0	60.0	60.0
Nozzle Dia., Dn (in.)	0.254	0.254	0.254
Oxygen, O2 (%)	14.0	13.5	15.5
Carbon Dioxide, CO2 (%)	15.5	14.2	12.5
Carbon Monoxide, CO (%)	0.0	0.0	0.0

Report Emission Criteria in ? 1 = lb/hr g = gr/dscf : L

Process Rate Units ? T = Ton/hr, L = Lbs/hr, C = Cans/min: T

Allowable Particulate Matter Emission Rate

LABORATORY RESULTS RUN RUN RUN
 1 2 3

GRAVIMETRIC ANALYSIS METHOD 5 :

Front Half Wash (FHW)	0.00410	0.00210	0.00150	grams
Filterable Sample (MF)	0.00140	0.00010	0.00120	
Condensable Sample (BHW)	0.00000	0.00000	0.00000	

SOURCE TEST CALCULATIONS

PLANT : RINKER / MIAMI, FL.
CEMENT KILN

RUN NO.: 1
DATE : SEPT 29, 2000

STD.TEMP, Tstd = 68 F	STATIC PRESS., Ps = -0.90 in. H2O
METER TEMP, Tm = 85 F	PITOT COFF., Cp = 0.840
STACK TEMP, Ts = 249.3 F	STACK I.D. = 132.40 inch
AVG.VEL.HEAD, dP = 0.637 in. H2O	DUCT LENGTH = inch
METER ORIFICE, dH = 1.54 in. H2O	DUCT WIDTH = inch
METER VOL., Vm = 44.500 Cu.Ft.	STACK AREA, As = 95.610 Sq.Ft.
METER COFF., Y = 1.000	TEST TIME = 60.00 min.
BAR. PRESS., Pb = 30.03 in.Hg	NOZZLE DIA. = 0.254 inch
COND.(Vlc) = 159.0 ml	NOZZLE DIA., An = 3.5E-04 Sq.Ft.

GAS ANALYSIS = 14.00 % O2	0.00 % CO
15.50 % CO2	70.50 % N2

$Vm(std) = [(T(std) + 460) / 29.92] \times Vm \times Y \times (Pb + (dH / 13.6)) / (Tm + 460)$	=	43.433	dscf
$Vw(std) = (8.9148 \times 10e-5) \times (Tstd + 460) \times Vlc$	=	7.484	scf
$Bws = Vw(std) / (Vm(std) + Vw(std))$	=	0.147	Lower Bws value used.
$Bws @ \text{Saturated Conditions} = \text{Vapor Press. of H2O @ Dew Point Temp.} / (Ps, \text{ in.Hg.})$	=	1.000	
$\%EA = (\%O2 - 0.5\%CO) / (0.264\%N2 - (\%O2 - 0.5\%CO)) \times 100$	=	303.56	
$Md = (.44 \times \%CO2) + (.32 \times \%O2) + [.28 \times (\%N2 + \%CO)]$	=	31.04	
$Ms = (Md \times (1 - Bws)) + (18.0 \times Bws)$	=	29.12	
$P(stack) = Pbar + (Ps / 13.6)$	=	29.96	in. Hg
$vs = 85.49 \times CP \times (Sq.Rt.dP) \times [Sq.Rt.(Ts + 460) / (Ms \times P(stack))]$	=	51.69	ft/sec
$Qs = vs \times As \times 60$	=	296,499	acf/min
$Qs(std) = Qs \times (1 - Bws) \times ((Tstd + 460) / (Ts + 460)) \times (P(stack) / 29.92)$	=	188,560	dscf/min
$I = (Ts + 460) \times [(0.002669 \times Vlc) + (Vm(std) / (T(std) + 460) / 29.92) \times 100 / [\text{Time} \times P(stack) \times An \times vs \times 60]$	=	104.32	%

SOURCE TEST CALCULATIONS

PLANT : RINKER / MIAMI, FL.
CEMENT KILN

RUN NO.: 2
DATE : SEPT 29, 2000

STD. TEMP, Tstd = 68 F	STATIC PRESS., Ps = -0.90 in. H2O
METER TEMP, Tm = 92.08 F	PITOT COFF., Cp = 0.840
STACK TEMP, Ts = 249.0 F	STACK I.D. = 132.40 inch
AVG. VEL. HEAD, dP = 0.640 in. H2O	DUCT LENGTH = inch
METER ORIFICE, dH = 1.52 in. H2O	DUCT WIDTH = inch
METER VOL., Vm = 44.670 Cu.Ft.	STACK AREA, As = 95.610 Sq.Ft.
METER COFF., Y = 1.000	TEST TIME = 60.00 min.
BAR. PRESS., Pb = 30.03 in.Hg	NOZZLE DIA. = 0.254 inch
COND.(Vlc) = 142.0 ml	NOZZLE DIA., An = 3.5E-04 Sq.Ft.

GAS ANALYSIS = 13.50 % O2	0.00 % CO
14.20 % CO2	72.30 % N2

$Vm(std) = [T(std) + 460 / 29.92] \times Vm \times Y \times (Pb + (dH / 13.6)) / (Tm + 460) \dots\dots$	=	43.038	dscf
$Vw(std) = (8.9148 \times 10e-5) \times (Tstd + 460) \times Vlc$	=	6.684	scf
$Bws = Vw(std) / (Vm(std) + Vw(std)) \dots\dots\dots$	=	0.134	Lower Bws value used.
$Bws @ \text{Saturated Conditions} = \text{Vapor Press. of H2O @ Dew Point Temp.} / (Ps, \text{in.Hg.}) \dots\dots\dots$	=	1.000	
$\%EA = (\%O2 - 0.5\%CO) / (0.264\%N2 - (\%O2 - 0.5\%CO)) \times 100 =$		241.62	
$Md = (.44 \times \%CO2) + (.32 \times \%O2) + [.28 \times (\%N2 + \%CO)] =$		30.81	
$Ms = (Md \times (1 - Bws)) + (18.0 \times Bws) \dots\dots\dots$	=	29.09	
$P(stack) = Pbar + (Ps / 13.6) \dots\dots\dots$	=	29.96	in. Hg
$vs = 85.49 \times CP \times (Sq.Rt.dP) \times [Sq.Rt.(Ts + 460) / (Ms \times P(stack))] \dots\dots\dots$	=	51.81	ft/sec
$Qs = vs \times As \times 60 \dots\dots\dots$	=	297,215	acf/min
$Qs(std) = Qs \times (1 - Bws) \times ((Tstd + 460) / (Ts + 460)) \times (P(stack) / 29.92) \dots\dots\dots$	=	191,866	dscf/min
$I = (Ts + 460) \times [(0.002669 \times Vlc) + (Vm(std) / (T(std) + 460) / 29.92)] \times 100 / [Time \times P(stack) \times An \times vs \times 60] \dots\dots\dots$	=	101.59	%

SOURCE TEST CALCULATIONS

PLANT : RINKER / MIAMI, FL.
CEMENT KILN

RUN NO.: 3
DATE : SEPT 29, 2000

STD. TEMP, Tstd = 68 F	STATIC PRESS., Ps = -0.90 in. H2O
METER TEMP, Tm = 91.67 F	PITOT COFF., Cp = 0.840
STACK TEMP, Ts = 375.6 F	STACK I.D. = 132.40 inch
AVG. VEL. HEAD, dP = 0.951 in. H2O	DUCT LENGTH = inch
METER ORIFICE, dH = 2.01 in. H2O	DUCT WIDTH = inch
METER VOL., Vm = 51.523 Cu.Ft.	STACK AREA, As = 95.610 Sq.Ft.
METER COFF., Y = 1.000	TEST TIME = 60.00 min.
BAR. PRESS., Pb = 30.03 in.Hg	NOZZLE DIA. = 0.254 inch
COND.(Vlc) = 94.0 ml	NOZZLE DIA., An = 3.5E-04 Sq.Ft.

GAS ANALYSIS = 15.50 % O2	0.00 % CO
12.50 % CO2	72.00 % N2

$Vm(std) = [T(std) + 460 / 29.92] \times Vm \times Y \times (Pb + (dH / 13.6)) / (Tm + 460) \dots\dots$	=	49.737	dscf
$Vw(std) = (8.9148 \times 10e-5) \times (Tstd + 460) \times Vlc$	=	4.425	scf
$Bws = Vw(std) / (Vm(std) + Vw(std)) \dots\dots\dots$	=	0.082	Lower Bws value used.
$Bws @ \text{Saturated Conditions} = \text{Vapor Press. of H2O @ Dew Point Temp.} / (Ps, \text{ in.Hg.}) \dots\dots\dots$	=	1.000	
$\%EA = (\%O2 - 0.5\%CO) / (0.264\%N2 - (\%O2 - 0.5\%CO)) \times 100 =$		441.85	
$Md = (.44 \times \%CO2) + (.32 \times \%O2) + [.28 \times (\%N2 + \%CO)] =$		30.62	
$Ms = (Md \times (1 - Bws)) + (18.0 \times Bws) \dots\dots\dots$	=	29.59	
$P(stack) = Pbar + (Ps / 13.6) \dots\dots\dots$	=	29.96	in. Hg
$vs = 85.49 \times CP \times (Sq.Rt.dP) \times [Sq.Rt.(Ts + 460) / (Ms \times P(stack))] \dots\dots\dots$	=	67.97	ft/sec
$Qs = vs \times As \times 60 \dots\dots\dots$	=	389,943	acf/min
$Qs(std) = Qs \times (1 - Bws) \times ((Tstd + 460) / (Ts + 460)) \times (P(stack) / 29.92) \dots\dots\dots$	=	226,605	dscf/min
$I = (Ts + 460) \times [(0.002669 \times Vlc) + (Vm(std) / (T(std) + 460) / 29.92] \times 100 / [Time \times P(stack) \times An \times vs \times 60] \dots\dots\dots$	=	99.40	%

A. FIELD DATA SUMMARY

PLANT : RINKER / MIAMI, FL.
 CEMENT KILN
 DATE : SEPT 29, 2000

	RUN 1	RUN 2	RUN 3
Vlc = Vol water collected in train, ml	159.0	142.0	94.0
Vm = Sample gas vol, meter cond., acf	44.500	44.670	51.523
Y = Meter calibration factor	1.0000	1.0000	1.0000
Pbar = Barometric pressure, in. Hg	30.03	30.03	30.03
Pstatic = Stack static pressure, in. H2O	-0.90	-0.90	-0.90
dH = Avg meter pressure diff, in. H2O	1.54	1.52	2.01
Tm = Absolute meter temp., degrees R	545.0	552.1	551.7
Vm(std) = Sample gas vol, Std. cond., dscf	43.433	43.038	49.737
Bws = Water vapor in gas stream, fraction	0.147	0.134	0.082
MF = Moisture factor (1 - Bws)	0.853	0.866	0.918
CO2 = Carbon Dioxide, dry, volume %	15.50	14.20	12.50
O2 = Oxygen, dry, volume %	14.00	13.50	15.50
N2 = Nitrogen, dry volume %	70.50	72.30	72.00
Md = Molecular weight of stack gas, dry	31.04	30.81	30.62
Ms = Molecular weight of stack gas, wet	29.12	29.09	29.59
Cp = Pitot tube coefficient	0.84	0.84	0.84
Sq.Rt. dP = Avg. square root of each dP	0.7983	0.8000	0.9750
Ts = Absolute stack temp., degrees R	709.3	709.0	835.6
A = Area of stack, ft2	95.61	95.61	95.61
Qstd = Volumetric flowrate, dscfm	188,560	191,866	226,605
An = Nozzle area, ft2	3.52E-04	3.52E-04	3.52E-04
0 = Sample time, minutes	60.00	60.00	60.00
%I = Isokinetic variation, percent	104.32	101.59	99.40

B. PARTICULATE DATA SUMMARY

PLANT : RINKER / MIAMI, FL.
 CEMENT KILN
 DATE : SEPT 29, 2000

	RUN 1	RUN 2	RUN 3
Sample Weight (FHW + MF + BHW), mg	5.50	2.20	2.70
Meter Volume, standard cond., Vm(std)	43.433	43.038	49.737
Carbon Dioxide, percent	15.50	14.20	12.50
Oxygen, percent	14.00	13.50	15.50
Sample Concentration :			
gr/scf	0.0017	0.0007	0.0008
gr/dscf	0.0020	0.0008	0.0008
gr/dscf @ 0 % CO2	0.0015	0.0007	0.0008
gr/dscf @ 0 % O2	0.0059	0.0022	0.0032
ppm * MW (dry gas).....	107.5	43.4	46.1
ppm * MW @ 0% CO2	0.0	0.0	0.0
ppm * MW @ 0% O2	325.6	122.5	178.3

EMISSION RATE CALCULATIONS

PLANT :RINKER / MIAMI, FL.
CEMENT KILN

RUN NO.: 1
DATE : SEPT 29, 2000

STANDARD TEMP. : 68 F

Front Half Wash (FHW) 0.00410 grams | Vm(std) 43.433 ft3
Mass Filter (MF) 0.00140 grams | Vw(std) 7.484 ft3
Back Half Wash (BHW) 0.00000 grams | Qs(std) 188,560 dscfm
Vm(std) SO2 dscf | Bws 0.147
CO2 CORR 0.0 % | CO2 15.50 %
O2 CORR. 0.0 % | O2 14.00 %

F-FACTOR

10E6 x [3.64(%H) + 1.53(%C) + 0.57(%S) + 0.14(%N) -
0.46(%O2)] / (Btu/lb) x [(Tstd + 460)/528] dscf/MMBtu
FUEL USE

Use Rate (gal/ton) * Process Wt. (ton/hr) gal/hr
Heat Input = (Process Weight (ton/hr) x Heating MMBtu/hr
Value (Btu/gal) x Fuel Use Rate (gal/ton) / 1E6
TOTAL PARTICULATE

15.432 x (FHW + MF + BHW) / [(Vm(std) + Vw(std))] ... 0.0017 gr/scf
15.432 x (FHW + MF + BHW) / (Vm(std)) 0.0020 gr/dscf
gr/dscf x (12 / %CO2) 0.0015 @ 0% CO2
gr/dscf x [(20.9 - Oxygen corr.) / (20.9 - %O2)] ... 0.0059 @ 0% O2
0.00857 x Qs(std) x gr/dscf 3.16 lb/hr
F-Fac x 1.4286E-4 x [20.9 / (20.9-%O2)] x gr/dscf .. lb/MMBtu
Particulate (lb/hr) / Heat Input (MMBtu/hr) lb/MMBtu
TOTAL ACID MIST

[1.0811E-4 x (Vt - Vtb) x N x Vsol] / Vol(aloq) lb Acid Mist
[Acid Mist (lb) / Vm std (ft^3)] x Qs std x 60 ... lb/hr
[Acid Mist (lb) / Vm std (ft^3)] x F-Factor lb/MMBtu
SULFUR DIOXIDE (SO2)

[7.061E-5 x (Vt - Vtb) x N x Vsol] / Vol(aloq) lb SO2
[SO2 (lb) / Vm std (ft^3)] x Qs std (ft^3/min) x 60 lb/hr
[SO2 (lb) / Vm std (ft^3)] x F lb/MMBtu
[Mass SO2 (lb) x 385 / 64E+6 (ft^3/lb)] / Vm (std) ppm
ppm x 0.0 % Corr. / 15.5 % CO2 in Stack ppm @ 0% CO2
ppm x (20.9% - 0.0% O2 Corr)/(20.9% - 14.0% O2 Stack ppm @ 0% O2
SO2 (lb/hr / Heat Input) lb/MMBtu
HYDROGEN CHLORIDE DATA SUMMARY

[Mass HCl(mg) x 385 x 1E6] / [453600 x 36.5 x Vm(std) ppm
ppm x 0.0 % Corr. / 15.5 % CO2 in Stack ppm @ 0% CO2
ppm x (20.9% - 0.0% O2 Corr)/(20.9% - 15.5% O2 Stack ppm @ 0% O2
[Mass HCl(mg) x 60 x Qs / (Vm(std) x 453,600)]... lb/hr

EMISSION RATE CALCULATIONS

PLANT :RINKER / MIAMI, FL.
CEMENT KILN

RUN NO.: 2
DATE : SEPT 29, 2000

STANDARD TEMP. : 68 F

Front Half Wash (FHW) 0.00210 grams Vm(std) 43.038 ft3
Mass Filter (MF) 0.00010 grams Vw(std) 6.684 ft3
Back Half Wash (BHW) 0.00000 grams Qs(std) 191,866 dscfm
Vm(std) SO2 dscf Bws 0.134
CO2 CORR 0.0 % CO2 14.20 %
O2 CORR. 0.0 % O2 13.50 %

F-FACTOR

10E6 x [3.64(%H) + 1.53(%C) + 0.57(%S) + 0.14(%N) -
0.46(%O2)] / (Btu/lb) x [(Tstd + 460)/528] dscf/MMBtu
FUEL USE

Use Rate (gal/ton) * Process Wt. (ton/hr) gal/hr
Heat Input = (Process Weight (ton/hr) x Heating MMBtu/hr
Value (Btu/gal) x Fuel Use Rate (gal/ton) / 1E6
TOTAL PARTICULATE

15.432 x (FHW + MF + BHW) / [(Vm(std) + Vw(std))] ... 0.0007 gr/scf
15.432 x (FHW + MF + BHW) / (Vm(std)) 0.0008 gr/dscf
gr/dscf x (12 / %CO2) 0.0007 @ 0% CO2
gr/dscf x [(20.9 - Oxygen corr.) / (20.9 - %O2)] ... 0.0022 @ 0% O2
0.00857 x Qs(std) x gr/dscf 1.30 lb/hr
F-Fac x 1.4286E-4 x [20.9 / (20.9-%O2)] x gr/dscf .. lb/MMBtu
Particulate (lb/hr) / Heat Input (MMBtu/hr) lb/MMBtu
TOTAL ACID MIST

[1.0811E-4 x (Vt - Vtb) x N x Vsol] / Vol(aloq) lb Acid Mist
[Acid Mist (lb) / Vm std (ft^3)] x Qs std x 60 ... lb/hr
[Acid Mist (lb) / Vm std (ft^3)] x F-Factor lb/MMBtu
SULFUR DIOXIDE (SO2)

[7.061E-5 x (Vt - Vtb) x N x Vsol] / Vol(aloq) . lb SO2
[SO2 (lb) / Vm std (ft^3)] x Qs std (ft^3/min) x 60 lb/hr
[SO2 (lb) / Vm std (ft^3)] x F lb/MMBtu
[Mass SO2 (lb) x 385 / 64E+6 (ft^3/lb)] / Vm (std) ppm
ppm x 0.0 % Corr. / 15.5 % CO2 in Stack ppm @ 0% CO2
ppm x (20.9% - 0.0% O2 Corr)/(20.9% - 15.5% O2 Stack ppm @ 0% O2
SO2 (lb/hr / Heat Input) lb/MMBtu
HYDROGEN CHLORIDE DATA SUMMARY

[Mass HCl(mg) x 385 x 1E6] / [453600 x 36.5 x Vm(std) ppm
ppm x 0.0 % Corr. / 14.2 % CO2 in Stack ppm @ 0% CO2
ppm x (20.9% - 0.0% O2 Corr)/(20.9% - 14.2% O2 Stack ppm @ 0% O2
[Mass HCl(mg) x 60 x Qs / (Vm(std) x 453,600)]... lb/hr

EMISSION RATE CALCULATIONS

PLANT :RINKER / MIAMI, FL.
CEMENT KILN

RUN NO.: 3
DATE : SEPT 29, 2000

STANDARD TEMP. : 68 F

Front Half Wash (FHW) 0.00150 grams | Vm(std) 49.737 ft3
Mass Filter (MF) 0.00120 grams | Vw(std) 4.425 ft3
Back Half Wash (BHW) 0.00000 grams | Qs(std) 226,605 dscfm
Vm(std) SO2 dscf | Bws 0.082
CO2 CORR 0.0 % | CO2 12.50 %
O2 CORR. 0.0 % | O2 15.50 %

F-FACTOR

10E6 x [3.64(%H) + 1.53(%C) + 0.57(%S) + 0.14(%N) -
0.46(%O2)] / (Btu/lb) x [(Tstd + 460)/528] dscf/MMBtu
FUEL USE

Use Rate (gal/ton) * Process Wt. (ton/hr) gal/hr
Heat Input = (Process Weight (ton/hr) x Heating MMBtu/hr
Value (Btu/gal) x Fuel Use Rate (gal/ton) / 1E6

TOTAL PARTICULATE

15.432 x (FHW + MF + BHW) / [(Vm(std) + Vw(std)] ... 0.0008 gr/scf
15.432 x (FHW + MF + BHW) / (Vm(std) 0.0008 gr/dscf
gr/dscf x (12 / %CO2) 0.0008 @ 0% CO2
gr/dscf x [(20.9 - Oxygen corr.) / (20.9 - %O2)] ... 0.0032 @ 0% O2
0.00857 x Qs(std) x gr/dscf 1.63 lb/hr
F-Fac x 1.4286E-4 x [20.9 / (20.9-%O2)] x gr/dscf .. lb/MMBtu
Particulate (lb/hr) / Heat Input (MMBtu/hr) lb/MMBtu

TOTAL ACID MIST

[1.0811E-4 x (Vt - Vtb) x N x Vsol] / Vol(aloq) lb Acid Mist
[Acid Mist (lb) / Vm std (ft^3)] x Qs std x 60 ... lb/hr
[Acid Mist (lb) / Vm std (ft^3)] x F-Factor lb/MMBtu

SULFUR DIOXIDE (SO2)

[7.061E-5 x (Vt - Vtb) x N x Vsol] / Vol(aloq) . lb SO2
[SO2 (lb) / Vm std (ft^3)] x Qs std (ft^3/min) x 60 lb/hr
[SO2 (lb) / Vm std (ft^3)] x F lb/MMBtu
[Mass SO2 (lb) x 385 / 64E+6 (ft^3/lb)] / Vm (std) ppm
ppm x 0.0 % Corr. / 15.5 % CO2 in Stack ppm @ 0% CO2
ppm x (20.9% - 0.0% O2 Corr)/(20.9% - 15.5% O2 Stack ppm @ 0% O2
SO2 (lb/hr / Heat Input) lb/MMBtu

HYDROGEN CHLORIDE DATA SUMMARY

[Mass HCl(mg) x 385 x 1E6] / [453600 x 36.5 x Vm(std) ppm
ppm x 0.0 % Corr. / 12.5 % CO2 in Stack ppm @ 0% CO2
ppm x (20.9% - 0.0% O2 Corr)/(20.9% - 12.5% O2 Stack ppm @ 0% O2
[Mass HCl(mg) x 60 x Qs / (Vm(std) x 453,600)]... lb/hr

KOOGLER AND ASSOCIATES, ENVIRONMENTAL SERVICES
SUMMARY OF VISIBLE EMISSIONS
FOR 60-MINUTES

PLANT : RINKER / MIAMI, FL.
SOURCE : CEMENT KILN
DATE : SEPT. 29, 2000
TIME : 08:23 TO 09:23

		SECONDS / 0	15	30	45
		----- OPACITY (%) -----			
MINUTES /					
	1	0	0	0	0
	2	0	0	0	0
	3	0	0	0	0
	4	0	0	0	0
	5	0	0	0	0
	6	0	0	0	0
	7	0	0	0	0
	8	0	0	0	0
	9	0	0	0	0
	10	0	0	0	0
	11	0	0	0	0
	12	0	0	0	0
	13	0	0	0	0
	14	0	0	0	0
	15	0	0	0	0
	16	0	0	0	0
	17	0	0	0	0
	18	0	0	0	0
	19	0	0	0	0
	20	0	0	0	0
	21	0	0	0	0
	22	0	0	0	0
	23	0	0	0	0
	24	0	0	0	0
	25	0	0	0	0
	26	0	0	0	0
	27	0	0	0	0
	28	0	0	0	0
	29	0	0	0	0
	30	0	0	0	0

KOOGLER AND ASSOCIATES, ENVIRONMENTAL SERVICES
SUMMARY OF VISIBLE EMISSIONS
FOR 60-MINUTES

PLANT : RINKER / MIAMI, FL.
SOURCE: CEMENT KILN
DATE : SEPT. 29, 2000
TIME : 08:23 TO 09:23

SECONDS	/	0	15	30	45
		OPACITY (%)			
31		0	0	0	0
32		0	0	0	0
33		0	0	0	0
34		0	0	0	0
35		0	0	0	0
36		0	0	0	0
37		0	0	0	0
38		0	0	0	0
39		0	0	0	0
40		0	0	0	0
41		0	0	0	0
42		0	0	0	0
43		0	0	0	0
44		0	0	0	0
45		0	0	0	0
46		0	0	0	0
47		0	0	0	0
48		0	0	0	0
49		0	0	0	0
50		0	0	0	0
51		0	0	0	0
52		0	0	0	0
53		0	0	0	0
54		0	0	0	0
55		0	0	0	0
56		0	0	0	0
57		0	0	0	0
58		0	0	0	0
59		0	0	0	0
60		0	0	0	0

AVERAGE OPACITY: 0.0 %

MAXIMUM OPACITY: 0 %

KOOGLER AND ASSOCIATES, ENVIRONMENTAL SERVICES
 SIX-MINUTE AVERAGES OF VISIBLE EMISSIONS
 FOR 60-MINUTES

PLANT : RINKER / MIAMI, FL.
 SOURCE: CEMENT KILN
 DATE : SEPT. 29, 2000
 TIME : 08:23 TO 09:23

MINUTES	--- SIX-MINUTE ROLLING AVERAGES ---			
	----- OPACITY (%) -----			
1	-	-	-	-
2	-	-	-	-
3	-	-	-	-
4	-	-	-	-
5	-	-	-	-
6	-	-	-	0.0
7	0.0	0.0	0.0	0.0
8	0.0	0.0	0.0	0.0
9	0.0	0.0	0.0	0.0
10	0.0	0.0	0.0	0.0
11	0.0	0.0	0.0	0.0
12	0.0	0.0	0.0	0.0
13	0.0	0.0	0.0	0.0
14	0.0	0.0	0.0	0.0
15	0.0	0.0	0.0	0.0
16	0.0	0.0	0.0	0.0
17	0.0	0.0	0.0	0.0
18	0.0	0.0	0.0	0.0
19	0.0	0.0	0.0	0.0
20	0.0	0.0	0.0	0.0
21	0.0	0.0	0.0	0.0
22	0.0	0.0	0.0	0.0
23	0.0	0.0	0.0	0.0
24	0.0	0.0	0.0	0.0
25	0.0	0.0	0.0	0.0
26	0.0	0.0	0.0	0.0
27	0.0	0.0	0.0	0.0
28	0.0	0.0	0.0	0.0
29	0.0	0.0	0.0	0.0
30	0.0	0.0	0.0	0.0

KOOGLER AND ASSOCIATES, ENVIRONMENTAL SERVICES
SIX-MINUTE AVERAGES OF VISIBLE EMISSIONS
FOR 60-MINUTES

PLANT : RINKER / MIAMI, FL.
SOURCE: CEMENT KILN
DATE : SEPT. 29, 2000
TIME : 08:23 TO 09:23

MINUTES	--- SIX-MINUTE ROLLING AVERAGES ---			
	----- OPACITY (%) -----			
31	0.0	0.0	0.0	0.0
32	0.0	0.0	0.0	0.0
33	0.0	0.0	0.0	0.0
34	0.0	0.0	0.0	0.0
35	0.0	0.0	0.0	0.0
36	0.0	0.0	0.0	0.0
37	0.0	0.0	0.0	0.0
38	0.0	0.0	0.0	0.0
39	0.0	0.0	0.0	0.0
40	0.0	0.0	0.0	0.0
41	0.0	0.0	0.0	0.0
42	0.0	0.0	0.0	0.0
43	0.0	0.0	0.0	0.0
44	0.0	0.0	0.0	0.0
45	0.0	0.0	0.0	0.0
46	0.0	0.0	0.0	0.0
47	0.0	0.0	0.0	0.0
48	0.0	0.0	0.0	0.0
49	0.0	0.0	0.0	0.0
50	0.0	0.0	0.0	0.0
51	0.0	0.0	0.0	0.0
52	0.0	0.0	0.0	0.0
53	0.0	0.0	0.0	0.0
54	0.0	0.0	0.0	0.0
55	0.0	0.0	0.0	0.0
56	0.0	0.0	0.0	0.0
57	0.0	0.0	0.0	0.0
58	0.0	0.0	0.0	0.0
59	0.0	0.0	0.0	0.0
60	0.0	0.0	0.0	0.0

HIGHEST SIX-MINUTE ROLLING AVERAGE: 0.0 %

KOOGLER AND ASSOCIATES, ENVIRONMENTAL SERVICES
 SUMMARY OF VISIBLE EMISSIONS
 FOR 60-MINUTES

PLANT : RINKER / MIAMI, FL.
 SOURCE: CEMENT KILN
 DATE : SEPT. 29, 2000
 TIME : 09:55 TO 10:55

		SECONDS / 0	15	30	45
		----- OPACITY (%) -----			
MINUTES /					
1		0	0	0	0
2		0	0	0	0
3		0	0	0	0
4		0	0	0	0
5		0	0	0	0
6		0	0	0	0
7		0	0	0	0
8		0	0	0	0
9		0	0	0	0
10		0	0	0	0
11		0	0	0	0
12		0	0	0	0
13		0	0	0	0
14		0	0	0	0
15		0	0	0	0
16		0	0	0	0
17		0	0	0	0
18		0	0	0	0
19		0	0	0	0
20		0	0	0	0
21		0	0	0	0
22		0	0	0	0
23		0	0	0	0
24		0	0	0	0
25		0	0	0	0
26		0	0	0	0
27		0	0	0	0
28		0	0	0	0
29		0	0	0	0
30		0	0	0	0

KOOGLER AND ASSOCIATES, ENVIRONMENTAL SERVICES
 SUMMARY OF VISIBLE EMISSIONS
 FOR 60-MINUTES

PLANT : RINKER / MIAMI, FL.
 SOURCE: CEMENT KILN
 DATE : SEPT. 29, 2000
 TIME : 09:55 TO 10:55

SECONDS	/	0	15	30	45
----- OPACITY (%) -----					
31		0	0	0	0
32		0	0	0	0
33		0	0	0	0
34		0	0	0	0
35		0	0	0	0
36		0	0	0	0
37		0	0	0	0
38		0	0	0	0
39		0	0	0	0
40		0	0	0	0
41		0	0	0	0
42		0	0	0	0
43		0	0	0	0
44		0	0	0	0
45		0	0	0	0
46		0	0	0	0
47		0	0	0	0
48		0	0	0	0
49		0	0	0	0
50		0	0	0	0
51		0	0	0	0
52		0	0	0	0
53		0	0	0	0
54		0	0	0	0
55		0	0	0	0
56		0	0	0	0
57		0	0	0	0
58		0	0	0	0
59		0	0	0	0
60		0	0	0	0

AVERAGE OPACITY: 0.0 %

MAXIMUM OPACITY: 0 %

KOOGLER AND ASSOCIATES, ENVIRONMENTAL SERVICES
 SIX-MINUTE AVERAGES OF VISIBLE EMISSIONS
 FOR 60-MINUTES

PLANT : RINKER / MIAMI, FL.
 SOURCE: CEMENT KILN
 DATE : SEPT. 29, 2000
 TIME : 09:55 TO 10:55

MINUTES	--- SIX-MINUTE ROLLING AVERAGES ---			
	----- OPACITY (%) -----			
1	-	-	-	-
2	-	-	-	-
3	-	-	-	-
4	-	-	-	-
5	-	-	-	-
6	-	-	-	0.0
7	0.0	0.0	0.0	0.0
8	0.0	0.0	0.0	0.0
9	0.0	0.0	0.0	0.0
10	0.0	0.0	0.0	0.0
11	0.0	0.0	0.0	0.0
12	0.0	0.0	0.0	0.0
13	0.0	0.0	0.0	0.0
14	0.0	0.0	0.0	0.0
15	0.0	0.0	0.0	0.0
16	0.0	0.0	0.0	0.0
17	0.0	0.0	0.0	0.0
18	0.0	0.0	0.0	0.0
19	0.0	0.0	0.0	0.0
20	0.0	0.0	0.0	0.0
21	0.0	0.0	0.0	0.0
22	0.0	0.0	0.0	0.0
23	0.0	0.0	0.0	0.0
24	0.0	0.0	0.0	0.0
25	0.0	0.0	0.0	0.0
26	0.0	0.0	0.0	0.0
27	0.0	0.0	0.0	0.0
28	0.0	0.0	0.0	0.0
29	0.0	0.0	0.0	0.0
30	0.0	0.0	0.0	0.0

KOOGLER AND ASSOCIATES, ENVIRONMENTAL SERVICES
SIX-MINUTE AVERAGES OF VISIBLE EMISSIONS
FOR 60-MINUTES

PLANT : RINKER / MIAMI, FL.
SOURCE: CEMENT KILN
DATE : SEPT. 29, 2000
TIME : 09:55 TO 10:55

MINUTES	--- SIX-MINUTE ROLLING AVERAGES ---			
	----- OPACITY (%) -----			
31	0.0	0.0	0.0	0.0
32	0.0	0.0	0.0	0.0
33	0.0	0.0	0.0	0.0
34	0.0	0.0	0.0	0.0
35	0.0	0.0	0.0	0.0
36	0.0	0.0	0.0	0.0
37	0.0	0.0	0.0	0.0
38	0.0	0.0	0.0	0.0
39	0.0	0.0	0.0	0.0
40	0.0	0.0	0.0	0.0
41	0.0	0.0	0.0	0.0
42	0.0	0.0	0.0	0.0
43	0.0	0.0	0.0	0.0
44	0.0	0.0	0.0	0.0
45	0.0	0.0	0.0	0.0
46	0.0	0.0	0.0	0.0
47	0.0	0.0	0.0	0.0
48	0.0	0.0	0.0	0.0
49	0.0	0.0	0.0	0.0
50	0.0	0.0	0.0	0.0
51	0.0	0.0	0.0	0.0
52	0.0	0.0	0.0	0.0
53	0.0	0.0	0.0	0.0
54	0.0	0.0	0.0	0.0
55	0.0	0.0	0.0	0.0
56	0.0	0.0	0.0	0.0
57	0.0	0.0	0.0	0.0
58	0.0	0.0	0.0	0.0
59	0.0	0.0	0.0	0.0
60	0.0	0.0	0.0	0.0

HIGHEST SIX-MINUTE ROLLING AVERAGE: 0.0 %

KOOGLER AND ASSOCIATES, ENVIRONMENTAL SERVICES
SUMMARY OF VISIBLE EMISSIONS
FOR 60-MINUTES

PLANT : RINKER / MIAMI, FL.
SOURCE : CEMENT KILN
DATE : SEPT. 29, 2000
TIME : 11:26 TO 12:26

		SECONDS / 0	15	30	45
		----- OPACITY (%) -----			
MINUTES /					
	1	0	0	0	0
	2	0	0	0	0
	3	0	0	0	0
	4	0	0	0	0
	5	0	0	0	0
	6	0	0	0	0
	7	0	0	0	0
	8	0	0	0	0
	9	0	0	0	0
	10	0	0	0	0
	11	0	0	0	0
	12	0	0	0	0
	13	0	0	0	0
	14	0	0	0	0
	15	0	0	0	0
	16	0	0	0	0
	17	0	0	0	0
	18	0	0	0	0
	19	0	0	0	0
	20	0	0	0	0
	21	0	0	0	0
	22	0	0	0	0
	23	0	0	0	0
	24	0	0	0	0
	25	0	0	0	0
	26	0	0	0	0
	27	0	0	0	0
	28	0	0	0	0
	29	0	0	0	0
	30	0	0	0	0

KOOGLER AND ASSOCIATES, ENVIRONMENTAL SERVICES
 SUMMARY OF VISIBLE EMISSIONS
 FOR 60-MINUTES

PLANT : RINKER / MIAMI, FL.
 SOURCE: CEMENT KILN
 DATE : SEPT. 29, 2000
 TIME : 11:26 TO 12:26

SECONDS	0	15	30	45
----- OPACITY (%) -----				
31	0	0	0	0
32	0	0	0	0
33	0	0	0	0
34	0	0	0	0
35	0	0	0	0
36	0	0	0	0
37	0	0	0	0
38	0	0	0	0
39	0	0	0	0
40	0	0	0	0
41	0	0	0	0
42	0	0	0	0
43	0	0	0	0
44	0	0	0	0
45	0	0	0	0
46	0	0	0	0
47	0	0	0	0
48	0	0	0	0
49	0	0	0	0
50	0	0	0	0
51	0	0	0	0
52	0	0	0	0
53	0	0	0	0
54	0	0	0	0
55	0	0	0	0
56	0	0	0	0
57	0	0	0	0
58	0	0	0	0
59	0	0	0	0
60	0	0	0	0

AVERAGE OPACITY: 0.0 %

MAXIMUM OPACITY: 0 %

KOOGLER AND ASSOCIATES, ENVIRONMENTAL SERVICES
 SIX-MINUTE AVERAGES OF VISIBLE EMISSIONS
 FOR 60-MINUTES

PLANT : RINKER / MIAMI, FL.
 SOURCE: CEMENT KILN
 DATE : SEPT. 29, 2000
 TIME : 11:26 TO 12:26

MINUTES	--- SIX-MINUTE ROLLING AVERAGES ---			
	----- OPACITY (%) -----			
1	-	-	-	-
2	-	-	-	-
3	-	-	-	-
4	-	-	-	-
5	-	-	-	-
6	-	-	-	0.0
7	0.0	0.0	0.0	0.0
8	0.0	0.0	0.0	0.0
9	0.0	0.0	0.0	0.0
10	0.0	0.0	0.0	0.0
11	0.0	0.0	0.0	0.0
12	0.0	0.0	0.0	0.0
13	0.0	0.0	0.0	0.0
14	0.0	0.0	0.0	0.0
15	0.0	0.0	0.0	0.0
16	0.0	0.0	0.0	0.0
17	0.0	0.0	0.0	0.0
18	0.0	0.0	0.0	0.0
19	0.0	0.0	0.0	0.0
20	0.0	0.0	0.0	0.0
21	0.0	0.0	0.0	0.0
22	0.0	0.0	0.0	0.0
23	0.0	0.0	0.0	0.0
24	0.0	0.0	0.0	0.0
25	0.0	0.0	0.0	0.0
26	0.0	0.0	0.0	0.0
27	0.0	0.0	0.0	0.0
28	0.0	0.0	0.0	0.0
29	0.0	0.0	0.0	0.0
30	0.0	0.0	0.0	0.0

KOOGLER AND ASSOCIATES, ENVIRONMENTAL SERVICES
 SIX-MINUTE AVERAGES OF VISIBLE EMISSIONS
 FOR 60-MINUTES

PLANT : RINKER / MIAMI, FL.
 SOURCE: CEMENT KILN
 DATE : SEPT. 29, 2000
 TIME : 11:26 TO 12:26

MINUTES	--- SIX-MINUTE ROLLING AVERAGES ---			
	----- OPACITY (%) -----			
31	0.0	0.0	0.0	0.0
32	0.0	0.0	0.0	0.0
33	0.0	0.0	0.0	0.0
34	0.0	0.0	0.0	0.0
35	0.0	0.0	0.0	0.0
36	0.0	0.0	0.0	0.0
37	0.0	0.0	0.0	0.0
38	0.0	0.0	0.0	0.0
39	0.0	0.0	0.0	0.0
40	0.0	0.0	0.0	0.0
41	0.0	0.0	0.0	0.0
42	0.0	0.0	0.0	0.0
43	0.0	0.0	0.0	0.0
44	0.0	0.0	0.0	0.0
45	0.0	0.0	0.0	0.0
46	0.0	0.0	0.0	0.0
47	0.0	0.0	0.0	0.0
48	0.0	0.0	0.0	0.0
49	0.0	0.0	0.0	0.0
50	0.0	0.0	0.0	0.0
51	0.0	0.0	0.0	0.0
52	0.0	0.0	0.0	0.0
53	0.0	0.0	0.0	0.0
54	0.0	0.0	0.0	0.0
55	0.0	0.0	0.0	0.0
56	0.0	0.0	0.0	0.0
57	0.0	0.0	0.0	0.0
58	0.0	0.0	0.0	0.0
59	0.0	0.0	0.0	0.0
60	0.0	0.0	0.0	0.0

HIGHEST SIX-MINUTE ROLLING AVERAGE: 0.0 %

VISIBLE EMISSIONS EVALUATOR

This is to certify that

Glen Haven

met the specifications of Federal Reference Method 9 and qualified as a visible emissions evaluator. Maximum deviation on white and black smoke did not exceed 7.5% opacity and no single error exceeding 15% opacity was incurred during the certification test conducted by Eastern Technical Associates of Raleigh, North Carolina. This certificate is valid for six months from date of issue.

278546

Certificate Number

Jacksonville, Florida

Location

June 7, 2000

Date of Issue


President


Director of Training

FIELD AND LABORATORY DATA SHEETS



Plant: Rinker - Miami
 Sample Loc.: Cement Kiln
 Control Type: Batch
 Sample Type: Palt
 Date: 9-29-00 Run No.: 1
 Time Start: 0823 Time End: 0928
 Sample Time: 5 min/port 60 total min.
 Dry Bulb: °F Wet Bulb: °F VP @ DP:
 Bar. Pressure 30.03 Hg Stack Press.: 29.96 Hg Ps: 29.0 H₂O
 Moisture: 12 % FDA: Gas Density Factor:
 Temperature: 78 °F Wind Dir.: E Wind Speed: 2-4
 Weather: cloudy Thermocouple Readout: KA-2
 Sample Box #: KA-2 Meter Box No.: KA-2
 Meter Y: 1.000 @ Delta H: 1.52 Pitot Corr.: 0.84
 Nozzle Diameter: 0.254 in. Probe Length: 6.5 ft
 Probe Heater Setting: 2 Nomograph Cf: 2.4
 Stack Dimensions: ~~116.5~~ 132.4 in
 Stack Area: ~~1046~~ 95.61 ft²
 Effective Stack Area: ~~1046~~ 95.61 ft²
 Stack Height: ft

Stack Dimensions

Material Processing Rate:
 Final Gas Meter Reading: 1042.700 ft³
 Initial Gas Meter Reading: 998.200 ft³
 Total Metered Gas Volume: 445.500 ft³
 Condensate Gain in Impingers: 150 mL
 Weight Gain in Silica Gel: 9 g
 Total Moisture Gain: 157 mL
 Silica Gel Container No.: 39
 Filter Number: 2610

Leak Check - Meter Box
 Initial: 0.000 cfm @ 15 in. H₂O
 Final: 0.000 cfm @ 5 in. H₂O

Leak Check - Pitot Tubes
 Impact 3 "H₂O for 15 sec: Stable Leak
 Static 3 "H₂O for 15 sec: Stable Leak



Test Conducted By: R Paul - A Bell
A Haven
 Stack Test Observers: O₂ % - 14.0
CO₂ % - 15.5

Port and Traverse Point No.	Distance from Inside Stack Wall (in.)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head (H ₂ O)	Meter Orifice Pressure Difference (H ₂ O)		Stack Gas Temperature (F)	Sample Box Temperature (F)	Last Impinger Temperature (F)	Meter Temperature (F)	Vacuum on Sample Train (Hg)	Oxygen Meter Reading (% O ₂)
					Calculated	Actual						
Average												
1-1	6.01		98.2	0.71	1.7	1.7	248	230	67	78	3	
2	19.9		1002.2	0.66	1.58	1.58	253	242	47	79	3	
3	40.4		51.8	0.52	1.25	1.25	248	253	47	80	3	
2-4			9.2	0.80	1.92	1.92	254	262	50	82	4	
2			13.4	0.66	1.58	1.58	253	245	48	84	3	
3			17.1	0.53	1.27	1.27	248	252	49	85	3	
3-1			20.5	0.76	1.82	1.82	251	260	52	87	4	
2			24.6	0.68	1.63	1.63	250	252	49	88	4	

Plant: Rinker - Miami
 Sample Loc.: Cement Kiln
 Control Type: Bag house
 Sample Type: Dust
 Date: 9-29-00 Run No.: 2
 Time Start: 0955 Time End: 1100
 Sample Time: 5 min/port 60 total min.
 Dry Bulb: °F Wet Bulb: °F VP @ DP:
 Bar. Pressure 30.03 Hg Stack Press.: 29.96 Hg Ps: 0.90 H₂O
 Moisture: 14 % FDA: Gas Density Factor:
 Temperature: 89 °F Wind Dir.: E Wind Speed: 5-10
 Weather: Cloudy Thermocouple Readout: KA-2
 Sample Box #: KA2 Meter Box No.: KA2
 Meter Y: 1000 @ Delta H: 1.52 Pitot Corr.: 0.84
 Nozzle Diameter: 0.254 in. Probe Length: 6.11 ft
 Probe Heater Setting: 2 Nomograph Ct: 2.36
 Stack Dimensions: 132.4 in Umbilical: 100'
 Stack Area: 95.61 ft² Thermocouple
 Effective Stack Area: 95.61 ft² Probe No.: KA-38
 Stack Height: ft Pitot Tube: KASS II

Stack Dimensions

Material Processing Rate:
 Final Gas Meter Reading: 87,670 ft³
 Initial Gas Meter Reading: 43,000 ft³
 Total Metered Gas Volume: 44,670 ft³
 Condensate Gain in Impingers: 135 mL
 Weight Gain in Silica Gel: 7 g
 Total Moisture Gain: 192 mL
 Silica Gel Container No.: 4
 Filter Number: 2641

Leak Check - Meter Box
 Initial: 0.000 cfm @ 15 in. H₂O
 Final: 0.001 cfm @ 6 in. H₂O

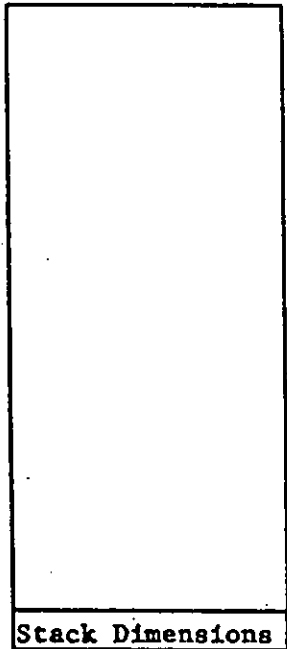
Leak Check - Pitot Tubes
 Impact 3 H₂O for 15 sec: Stable Leak
 Static 3 H₂O for 15 sec: Stable Leak



Test Conducted By: R Paul - J Bell
J Haven
 Stack Test Observers: O₂ % - 13.5
CO₂ % - 14.2

Port and Traverse Point No.	Distance from Inside Stack Wall (ft.)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head (H ₂ O)	Meter Orifice Pressure Difference (H ₂ O)		Stack Gas Temperature (F)	Sample Box Temperature (F)	Last Impinger Temperature (F)	Meter Temperature (F)	Vacuum on Sample Train (Hg)	Oxygen Meter Reading (% O ₂)
					Calculated	Actual						
Average												
1-1			430	0.68	1.6	1.6	243	233	67	89	4	
2			46.8	0.65	1.53	1.53	244	239	56	89	4	
3			50.5	0.51	1.2	1.2	242	248	47	90	3	
2-1			53.8	0.73	1.72	1.72	243	255	50	91	4	
2			57.8	0.64	1.51	1.51	246	260	48	92	4	
3			61.6	0.53	1.25	1.25	242	257	48	92	4	
3-1			65.0	0.69	1.63	1.63	246	266	50	93	4	
2			68.8	0.62	1.46	1.46	246	269	49	93	4	

Plant: Peabody - Miami
 Sample Loc.: Cement Kiln
 Control Type: Baghouse
 Sample Type: Dust
 Date: 9-29-00 Run No.: 3
 Time Start: 1127 Time End: 1231
 Sample Time: 5 min/port 60 total min.
 Dry Bulb: °F Wet Bulb: °F VP @ DP:
 Bar. Pressure 300.3 Hg Stack Press.: 299.12 Hg Ps: 290 H₂O
 Moisture: 13 % FDA: Gas Density Factor:
 Temperature: 85 °F Wind Dir.: E Wind Speed: 5-10
 Weather: Rain Thermocouple Readout: KA2
 Sample Box #: KA2 Meter Box No.: KA2
 Meter Y: 1.000 @ Delta H: 1.52 Pitot Corr.: 0.84
 Nozzle Diameter: 0.254 in. Probe Length: 6.0 ft
 Probe Heater Setting: 2 Nomograph Cf: 2.1
 Stack Dimensions: 132.4 in Umbilical: 100'
 Stack Area: 95.61 ft² Thermocouple
 Effective Stack Area: 95.61 ft² Probe No.: KA-38
 Stack Height: ft Pitot Tube: KA-55II



Material Processing Rate:
 Final Gas Meter Reading: 139.523 ft³
 Initial Gas Meter Reading: 88.000 ft³
 Total Metered Gas Volume: 51.523 ft³
 Condensate Gain in Impingers: 85 mL
 Weight Gain in Silica Gel: 9 g
 Total Moisture Gain: 94 mL
 Silica Gel Container No.: 10
 Filter Number: 2612

Leak Check - Meter Box
 Initial: 0.002 cfm @ 15 in. H₂O
 Final: 0.003 cfm @ 6 in. H₂O
 Leak Check - Pitot Tubes
 Impact 3 "H₂O for 15 sec: Stable Leak
 Static 3 "H₂O for 15 sec: Stable Leak



Test Conducted By: R Paul - A Bell
A Haven
 Stack Test Observers: O₂ % - 15.5
CO₂ % - 12.5

Port and Traverse Point No.	Distance from Inside Stack Wall (in.)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head (H ₂ O)	Meter Orifice Pressure Difference (H ₂ O)		Stack Gas Temperature (F)	Sample Box Temperature (F)	Last Impinger Temperature (F)	Meter Temperature (F)	Vacuum on Sample Train (Hg)	Oxygen Meter Reading (% O ₂)
					Calculated	Actual						
1-1			88.0	1.2	2.52	2.52	367	271	59	91	5	
2			92.8	0.94	1.97	1.97	366	236	47	90	5	
3			97.0	0.69	1.45	1.45	360	245	49	91	4	
2-1			100.7	1.1	2.31	2.31	379	271	52	92	5	
2			5.4	1.0	2.1	2.1	378	252	47	91	5	
3			9.8	0.81	1.7	1.7	375	235	47	92	4	
3-1			13.8	1.1	2.31	2.31	379	254	48	92	5	
2			18.4	0.75	2.0	2.0	380	240	49	92	5	

SAMPLING RATE CALCULATIONS

Date 9-29-00

Plant Name Rinker

Location Miami

Source Cement Kiln

- ΔH = Orifice Reading (Inches H_2O)
- D_n = Nozzle Diameter (Inches)
- ΔH_E = Meter Box Constant
- B_w = Moisture Fraction
- T_m = Meter Temperature ($^{\circ}F$)
- T_s = Stack Temperature ($^{\circ}F$)
- M_s = Wet Molecular Weight of Stack Gas (From Table)
- ΔP = Pitot Reading (Inches H_2O)

$T_s - 250$

$$\frac{T_m + 460}{M_s(T_s + 460)} (1 - B_w)^2 \Delta H_E (D_n)^4 17741 \Delta P = \Delta H$$

0.68
 0.64
 0.50

Moisture Fraction	M_s
0.0	29.0
0.05	28.5
0.10	27.9
0.15	27.4
0.20	26.8
0.25	26.2
0.30	25.7
0.35	25.2
0.40	24.6

543

~~710~~ (710) 19667

27.7

554

27.5 (710) 19525

553

276 (810) 22356

	Run 1	Run 2	Run 3
$\frac{T_m + 460}{M_s (T_s + 460)}$	= 0.02761	0.02838	0.02476
$\times (1 - B_w)^2$	= 0.7744	0.7396	0.7569
$\times \Delta H_E$	= 1.52	1.52	
$\times (D_n)^4$	= 0.00416	0.00416	
$\times 17741$	= 17741	17741	
$\times \Delta P$	= 2.4	2.36	2.1
	576.57		



CHAIN OF CUSTODY RECORD

Project Number

263-00-09

Project Name

Rinker

Sample Location

Miami, FL
Cement Keln

Sample Identification	Remarks
<u>1-RCM-P</u>	<u>Probe Wash Run 1</u>
<u>2-RCM-P</u>	<u>} } } 2</u>
<u>3-RCM-P</u>	<u>} } } 3</u>
<u>I</u>	<u>Filter Holder Run 1</u>
<u>II</u>	<u>} } } 2</u>
<u>III</u>	<u>} } } 3</u>
<u>39</u>	<u>Silica Gel Run 1</u>
<u>4</u>	<u>} } } 2</u>
<u>10</u>	<u>} } } 3</u>

Sampled By: (Signature) R Paul Date: 9-29-00 Time: See data

Relinquished By: (Sign) _____ Date: _____ Time: _____

Received By: (Sign) _____ Date: _____ Time: _____

Relinquished By: (Sign) _____ Date: _____ Time: _____

Received By: (Sign) _____ Date: _____ Time: _____

Relinquished By: (Sign) _____ Date: _____ Time: _____

Received By Lab: (Sign) R Paul Date: 9-29-00 Time: 2050

Sample Shipped VIA: _____ UPS _____ Fed Express _____ Bus

Shipping Bill Number: _____





KOOGLER & ASSOCIATES
ENVIRONMENTAL SERVICES
 4014 NW THIRTEENTH STREET
 GAINESVILLE, FLORIDA 32609
 904/377-5822 • FAX 377-7158

PARTICULATE LAB DATA SHEET

TEST DATE 9-29-00

PLANT NAME Reinbar

SOURCE Cement Kiln

	<u>Run 1</u>	<u>Run 2</u>	<u>Run 3</u>	<u>Blank</u>
Container No.	<u>102</u>	<u>KA-18</u>	<u>51</u>	<u>801</u>
Total Volume (ml)	<u>125</u>	<u>125</u>	<u>125</u>	<u>150</u>
Aliquot Evaporated (ml)	<u>125</u>	<u>125</u>	<u>125</u>	<u>150</u>
Final Weight (g)	<u>115.9845</u>	<u>100.9090</u>	<u>115.8714</u>	<u>100.5159</u>
Tare Weight (g)	<u>115.9804</u>	<u>100.9069</u>	<u>115.8699</u>	<u>100.5153</u>
Gross Weight Gained (g)	<u>115.9845</u> <u>0.0041</u>	<u>0.0021</u>	<u>0.0015</u>	<u>0.0006</u>
Average Blank (g)	<u>—</u>	<u>—</u>	<u>—</u>	<u>—</u>
Net Weight (g)	<u>0.0041</u>	<u>0.0021</u>	<u>0.0015</u>	<u>—</u>
Aliquot Factor	<u>x 1.0</u>	<u>x 1.0</u>	<u>x 1.0</u>	<u>x —</u>
Total Net Weight (mg)	<u>4.1</u>	<u>2.1</u>	<u>1.5</u>	<u>—</u>

Container No.	<u>1-14</u>	<u>2-14</u>	<u>3-14</u>	<u>BL-2</u>
Filter No.	<u>2610</u>	<u>2611</u>	<u>2612</u>	<u>2563</u>
Final Weight (g)	<u>0.4177</u>	<u>0.4161</u>	<u>0.4176</u>	<u>0.4149</u>
Tare Weight (g)	<u>0.4163</u>	<u>0.4160</u>	<u>0.4164</u>	<u>0.4150</u>
Gross Weight Gained (g)	<u>0.0014</u>	<u>0.0001</u>	<u>0.0012</u>	<u>-0.0001</u>
Average Blank (g)	<u>—</u>	<u>—</u>	<u>—</u>	<u>—</u>
Total Net Weight (mg)	<u>1.4</u>	<u>0.1</u>	<u>1.2</u>	<u>—</u>

Tare Balance Check

0.0 — 10.0 —
 1.0 — 50.0 —
 5.0 — 100.0 —
 T/H 77-44

Final Balance Check

0.0 — 10.0 —
 1.0 — 50.0 —
 5.0 — 100.0 —
 T/H 75-44

By R Paul

Date 10-1-00

By R Paul

Date 10-2-00



ENVIRONMENTAL SERVICES
4014 NW THIRTEENTH STREET
GAINESVILLE, FLORIDA 32609
904/377-5622 - FAX 377-7150

CONTINUED ON VEO FORM NUMBER 193

SOURCE NAME		OBSERVATION DATE				START TIME				STOP TIME			
CSR Rinker Materials		9/29/00				08:23				09:23			
ADDRESS		SEC		MIN		SEC		MIN		SEC		MIN	
Dade County		0	15	30	45	0	15	30	45	0	15	30	45
CITY	Miami	STATE	FL	ZIP		1	0	0	0	31	0	0	0
PHONE		SOURCE ID NUMBER				2	0	0	0	32	0	0	0
PROCESS EQUIPMENT	Cement Kiln	OPERATING MODE	200 TPH			3	0	0	0	33	0	0	0
CONTROL EQUIPMENT	Baghouse	OPERATING MODE				4	0	0	0	34	0	0	0
DESCRIBE EMISSION POINT	START Large silver stack north of preheater / STOP					5	0	0	0	35	0	0	0
HEIGHT ABOVE GROUND LEVEL	START ~ 325 STOP ~ 325	HEIGHT RELATIVE TO OBSERVER	START ~ 325 STOP ~ 325			6	0	0	0	36	0	0	0
DISTANCE FROM OBSERVER	START 800' STOP 800'	DIRECTION FROM OBSERVER	START 270 W STOP 270 W			7	0	0	0	37	0	0	0
DESCRIBE EMISSIONS	START clear/home STOP SAME					8	0	0	0	38	0	0	0
EMISSION COLOR	START none STOP none	PLUME TYPE: CONTINUOUS <input checked="" type="checkbox"/> FUGITIVE <input type="checkbox"/> INTERMITTENT <input type="checkbox"/>				9	0	0	0	39	0	0	0
WATER DROPLETS PRESENT:	NO <input checked="" type="checkbox"/> YES <input type="checkbox"/>	IF WATER DROPLET PLUME: ATTACHED <input type="checkbox"/> DETACHED <input type="checkbox"/>				10	0	0	0	40	0	0	0
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED	START Stack outlet STOP SAME					11	0	0	0	41	0	0	0
DESCRIBE BACKGROUND	START SKY STOP SKY					12	0	0	0	42	0	0	0
BACKGROUND COLOR	START white / STOP blue	SKY CONDITIONS	BROKEN START Scat. STOP Scat			13	0	0	0	43	0	0	0
WIND SPEED	START 1-4 STOP 1-4	WIND DIRECTION	SW to E START East STOP East			14	0	0	0	44	0	0	0
AMBIENT TEMP.	START 77 STOP 81	WET BULB TEMP.	75	RH percent	91%	15	0	0	0	45	0	0	0
<p>Source Layout Sketch</p> <p>control room - □</p> <p>Preheater Tower</p> <p>Emission Point</p> <p>old cement kilns</p> <p>Observers Position</p> <p>Sun Location Line 140°</p> <p>Plume and Stack</p> <p>1 - main office</p>					16	0	0	0	46	0	0	0	
					17	0	0	0	47	0	0	0	
					18	0	0	0	48	0	0	0	
					19	0	0	0	49	0	0	0	
					20	0	0	0	50	0	0	0	
					21	0	0	0	51	0	0	0	
					22	0	0	0	52	0	0	0	
					23	0	0	0	53	0	0	0	
					24	0	0	0	54	0	0	0	
					25	0	0	0	55	0	0	0	
					26	0	0	0	56	0	0	0	
					27	0	0	0	57	0	0	0	
28	0	0	0	58	0	0	0						
29	0	0	0	59	0	0	0						
30	0	0	0	60	0	0	0						
AVERAGE OPACITY FOR HIGHEST PERIOD					0%	NUMBER OF READINGS ABOVE 10% WERE 0							
RANGE OF OPACITY READINGS					0% MINIMUM	0% MAXIMUM							
OBSERVER'S NAME (PRINT)					Glen A. Haven								
OBSERVER'S SIGNATURE					Glen A. Haven								
DATE					9/29/00								
ORGANIZATION					K+A								
I HAVE RECEIVED A COPY OF THESE OPACITY OBSERVATIONS SIGNATURE					ETA								
DATE					6/00								
TITLE													
DATE													
VERIFIED BY													
DATE													



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CONTINUED ON VEO FORM NUMBER

2 of 3

SOURCE NAME			OBSERVATION DATE				START TIME		STOP TIME			
CSR Rinker			9/29/00				09:55		10:55			
ADDRESS			SEC				SEC		SEC			
			MIN	0	15	30	45	MIN	0	15	30	45
			1	0	0	0	0	31	0	0	0	0
			2	0	0	0	0	32	0	0	0	0
			3	0	0	0	0	33	0	0	0	0
			4	0	0	0	0	34	0	0	0	0
			5	0	0	0	0	35	0	0	0	0
			6	0	0	0	0	36	0	0	0	0
			7	0	0	0	0	37	0	0	0	0
			8	0	0	0	0	38	0	0	0	0
			9	0	0	0	0	39	0	0	0	0
			10	0	0	0	0	40	0	0	0	0
			11	0	0	0	0	41	0	0	0	0
			12	0	0	0	0	42	0	0	0	0
			13	0	0	0	0	43	0	0	0	0
			14	0	0	0	0	44	0	0	0	0
			15	0	0	0	0	45	0	0	0	0
			16	0	0	0	0	46	0	0	0	0
			17	0	0	0	0	47	0	0	0	0
			18	0	0	0	0	48	0	0	0	0
			19	0	0	0	0	49	0	0	0	0
			20	0	0	0	0	50	0	0	0	0
			21	0	0	0	0	51	0	0	0	0
			22	0	0	0	0	52	0	0	0	0
			23	0	0	0	0	53	0	0	0	0
			24	0	0	0	0	54	0	0	0	0
			25	0	0	0	0	55	0	0	0	0
			26	0	0	0	0	56	0	0	0	0
			27	0	0	0	0	57	0	0	0	0
			28	0	0	0	0	58	0	0	0	0
			29	0	0	0	0	59	0	0	0	0
			30	0	0	0	0	60	0	0	0	0
PROCESS EQUIPMENT Cement Kiln			OPERATING MODE 200 TPH									
CONTROL EQUIPMENT Baghouse			OPERATING MODE									
DESCRIBE EMISSION POINT START Round Silver Stack North of preheater / S.W.												
HEIGHT ABOVE GROUND LEVEL START ~ 325 STOP ~ 375			HEIGHT RELATIVE TO OBSERVER START 325 STOP 325									
DISTANCE FROM OBSERVER START ~ 80 STOP ~ 800			DIRECTION FROM OBSERVER START 280 W STOP 280 W									
DESCRIBE EMISSIONS START clear / none STOP same												
EMISSION COLOR START none STOP none			PLUME TYPE: CONTINUOUS <input checked="" type="checkbox"/> FUGITIVE <input type="checkbox"/> INTERMITTENT <input type="checkbox"/>									
WATER DROPLETS PRESENT: NO <input checked="" type="checkbox"/> YES <input type="checkbox"/>			IF WATER DROPLET PLUME: ATTACHED <input type="checkbox"/> DETACHED <input type="checkbox"/>									
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED START Stack outlet STOP same												
DESCRIBE BACKGROUND START SKY STOP SKY												
BACKGROUND COLOR White			SKY CONDITIONS START Scat, STOP Broken									
WIND SPEED START 1-5 STOP 1-5			WIND DIRECTION START NE STOP East									
AMBIENT TEMP. START 82 STOP 84			WET BULB TEMP. 77		RH, percent 80%							
<p>Source Layout Sketch</p> <p>Draw North Arrow</p> <p>preheater tower</p> <p>Emission Point</p> <p>control room</p> <p>Sun Wind → Plume and Stack</p> <p>Observers Position - old Kilns</p> <p>1140°</p> <p>Sun location Line</p> <p>main office</p>												
AVERAGE OPACITY FOR HIGHEST PERIOD 0%			NUMBER OF READINGS ABOVE 10% WERE 0									
RANGE OF OPACITY READINGS 0 MINIMUM 0 MAXIMUM												
OBSERVER'S NAME (PRINT) Glen A. Haven			OBSERVER'S SIGNATURE [Signature]				DATE 9/29/00					
COMMENTS Test concurrent w/ PM test #2 ATS 18°			ORGANIZATION K+A									
I HAVE RECEIVED A COPY OF THESE OPACITY OBSERVATIONS SIGNATURE			CERTIFIED BY ETA				DATE 6/00					
TITLE			DATE				VERIFIED BY		DATE			



ENVIRONMENTAL SERVICES
4011 NW THIRTEENTH STREET
GAINESVILLE, FLORIDA 32609
904/377-5622 - FAX 377-2154

CONTINUED ON VEO FORM NUMBER

3 of 3

SOURCE NAME			OBSERVATION DATE				START TIME		STOP TIME			
CSR Rinker			9/29/00				11:26		12:26			
ADDRESS			SEC				SEC					
			MIN	0	15	30	45	MIN	0	15	30	45
			1	0	0	0	0	31	0	0	0	0
			2	0	0	0	0	32	0	0	0	0
			3	0	0	0	0	33	0	0	0	0
			4	0	0	0	0	34	0	0	0	0
			5	0	0	0	0	35	0	0	0	0
			6	0	0	0	0	36	0	0	0	0
			7	0	0	0	0	37	0	0	0	0
			8	0	0	0	0	38	0	0	0	0
			9	0	0	0	0	39	0	0	0	0
			10	0	0	0	0	40	0	0	0	0
			11	0	0	0	0	41	0	0	0	0
			12	0	0	0	0	42	0	0	0	0
			13	0	0	0	0	43	0	0	0	0
			14	0	0	0	0	44	0	0	0	0
			15	0	0	0	0	45	0	0	0	0
			16	0	0	0	0	46	0	0	0	0
			17	0	0	0	0	47	0	0	0	0
			18	0	0	0	0	48	0	0	0	0
			19	0	0	0	0	49	0	0	0	0
			20	0	0	0	0	50	0	0	0	0
			21	0	0	0	0	51	0	0	0	0
			22	0	0	0	0	52	0	0	0	0
			23	0	0	0	0	53	0	0	0	0
			24	0	0	0	0	54	0	0	0	0
			25	0	0	0	0	55	0	0	0	0
			26	0	0	0	0	56	0	0	0	0
			27	0	0	0	0	57	0	0	0	0
			28	0	0	0	0	58	0	0	0	0
			29	0	0	0	0	59	0	0	0	0
			30	0	0	0	0	60	0	0	0	0
CITY Miami			STATE FL			ZIP						
PHONE			SOURCE ID NUMBER									
PROCESS EQUIPMENT Cement Kiln			OPERATING MODE 200 TPH									
CONTROL EQUIPMENT Baghouse			OPERATING MODE									
DESCRIBE EMISSION POINT START Round silver Stack north of Preheater / Stack STOP												
HEIGHT ABOVE GROUND LEVEL START ~325' STOP ~325'			HEIGHT RELATIVE TO OBSERVER START ~325' STOP ~325'									
DISTANCE FROM OBSERVER START ~800' STOP ~800'			DIRECTION FROM OBSERVER START 280° W STOP 280° W									
DESCRIBE EMISSIONS START Clear / none STOP Same												
EMISSION COLOR START none STOP none			PLUME TYPE: CONTINUOUS <input checked="" type="checkbox"/> FUGITIVE <input type="checkbox"/> INTERMITTENT <input type="checkbox"/>									
WATER DROPLETS PRESENT: NO <input checked="" type="checkbox"/> YES <input type="checkbox"/>			IF WATER DROPLET PLUME: ATTACHED <input type="checkbox"/> DETACHED <input type="checkbox"/>									
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED START Stack outlet STOP Same												
DESCRIBE BACKGROUND START SKY STOP SKY												
BACKGROUND COLOR START Grey STOP			SKY CONDITIONS START Overcast STOP									
WIND SPEED START 7-5 STOP			WIND DIRECTION START East STOP									
AMBIENT TEMP. START 80 STOP			WET BULB TEMP. 76			RH percent 84						
<p>Source Layout Sketch Draw North Arrow</p>												
AVERAGE OPACITY FOR HIGHEST PERIOD 0%			NUMBER OF READINGS ABOVE 10% WERE 0									
RANGE OF OPACITY READINGS 0% MINIMUM			0% MAXIMUM									
OBSERVER'S NAME (PRINT) Glen A. Haven												
COMMENTS VE Test concurrent with PM run #3 ATS 18°			OBSERVER'S SIGNATURE Glen A. Haven						DATE 9/29/00			
I HAVE RECEIVED A COPY OF THESE OPACITY OBSERVATIONS SIGNATURE			CERTIFIED BY ETA						DATE 6/00			
TITLE			DATE			VERIFIED BY			DATE			

PLANT INFORMATION

9/29/00 8am-1pm 1002 tons total (482,100 tons = 48,218 tons on the total 187)

200.6 tons per hour Kln Log



DATE TIME	MIN RUN TIME	MIN FLOW RATE	MIN FLOW RATE	PRECEDING RUN TIME	PUR. COAL TO MIN	W/ TO MIN	PUR. COAL TO W/DRIVER	BURNING RATE TEMPERATURE	CYCLONE 4 CORE PRESSURE	PRH DIVERTER GATE POSITION%	MIN FAN TOTAL TEMP	CYCLONE 1 INLET TEMPERATURE	CYCLONE 1 EXIT TEMP	CYCLONE 1 INLET PRESSURE	CYCLONE 2 INLET TEMPERATURE	CYCLONE 2 EXIT TEMP	CYCLONE 2 INLET PRESSURE	CYCLONE 3 INLET TEMPERATURE	CYCLONE 3 EXIT TEMP	CYCLONE 3 INLET PRESSURE	CYCLONE 4 INLET TEMPERATURE	CYCLONE 4 EXIT TEMP	CYCLONE 4 INLET PRESSURE	CYCLONE 4 EXIT PRESSURE
10/29/00 08:00:00	1921.2	200.6	480,487	2,781	0.04	0.07	0.73	2130	-12.17	48	136	797	797	-25.67	1009	1,068	-18.66	PN/A	1,207	1,165	-18.20	-18.83	1,488	1,204
10/29/00 08:05:00	1922.2	200.6	480,407	2,792	0.06	0.06	0.85	2182	-11.82	48	161	791	701	-25.19	1084	1,061	-18.08	PN/A	1,204	1,144	-14.88	-18.87	1,490	1,263
10/29/00 08:10:00	1923.2	200.6	480,308	2,783	0.06	0.01	0.83	2183	-11.84	48	162	792	701	-25.19	1083	1,061	-17.87	PN/A	1,204	1,143	-18.88	-18.87	1,490	1,263
10/29/00 08:15:00	1924.2	200.6	481,008	2,784	0.04	0.00	0.21	2181	-11.83	48	162	793	783	-25.18	1082	1,063	-17.93	PN/A	1,204	1,144	-14.34	-18.90	1,490	1,274
10/29/00 08:20:00	1928.2	200.6	481,280	2,785	0.01	0.00	0.24	2121	-12.87	48	160	793	708	-25.48	1087	1,064	-18.11	PN/A	1,204	1,148	-14.67	-18.88	1,481	1,283
10/29/00 08:25:00	1930.2	200.6	481,009	2,786	0.08	0.00	0.87	2123	-12.27	48	161	797	708	-25.64	1089	1,068	-18.41	PN/A	1,207	1,147	-18.08	-18.82	1,491	1,287
10/29/00 08:30:00	1937.2	200.6	481,899	2,787	0.08	0.00	0.83	2098	-12.17	41	161	798	709	-25.86	1088	1,067	-18.21	PN/A	1,209	1,148	-18.82	-18.83	1,491	1,283
10/29/00 08:35:00	1938.2	200.6	481,900	2,788	0.41	0.00	0.02	2083	-12.12	48	161	799	709	-25.88	1088	1,067	-18.12	PN/A	1,209	1,148	-14.44	-18.88	1,492	1,170
10/29/00 08:40:00	1939.2	200.6	482,100	2,788	0.47	0.00	0.12	2071	-12.11	48	160	712	712	-25.71	1083	1,070	-17.81	PN/A	1,201	1,158	-18.88	-18.83	1,483	1,219
10/29/00 08:45:00	1948.2	200.6	482,300	2,790	0.00	0.00	0.00	2077	-11.86	48	160	716	716	-25.43	1087	1,073	-17.82	PN/A	1,203	1,151	-18.37	-18.73	1,492	1,224
10/29/00 08:50:00	1941.2	200.6	482,301	2,791	0.00	0.00	0.83	2031	-11.88	48	160	713	713	-25.78	1088	1,071	-17.87	PN/A	1,203	1,150	-18.22	-18.77	1,482	1,231
10/29/00 08:55:00	1942.2	200.6	482,791	2,792	0.00	0.00	0.00	2077	-11.86	48	160	708	708	-24.94	1089	1,067	-18.01	PN/A	1,209	1,149	-18.94	-18.48	1,481	1,248
10/29/00 09:00:00	1943.2	200.6	482,802	2,793	0.47	0.00	0.00	2073	-11.74	48	172	708	708	-26.33	1088	1,068	-18.23	PN/A	1,208	1,148	-18.31	-18.48	1,491	1,279
10/29/00 09:05:00	1944.2	201.2	483,183	2,794	0.48	0.00	0.00	2111	-11.78	48	163	703	703	-25.30	1088	1,043	-18.04	PN/A	1,208	1,144	-18.20	-18.82	1,491	1,288
10/29/00 09:10:00	1945.2	200.3	483,384	2,795	0.52	0.00	0.00	2098	-12.87	41	163	704	704	-25.84	1087	1,064	-18.94	PN/A	1,207	1,143	-18.88	-18.84	1,491	1,274
10/29/00 09:15:00	1946.2	200.5	483,898	2,796	0.52	0.00	0.03	1987	-12.74	48	163	708	707	-27.83	1089	1,068	-20.88	PN/A	1,208	1,149	-18.47	-18.63	1,492	1,279
10/29/00 09:20:00	1947.2	200.9	483,712	2,797	0.48	0.00	0.28	1938	-13.12	48	163	711	711	-27.79	1081	1,068	-21.88	PN/A	1,201	1,148	-18.83	-17.18	1,493	1,280
10/29/00 09:25:00	1948.2	200.5	483,917	2,798	0.48	0.00	0.47	1914	-12.22	48	168	717	716	-28.18	1088	1,071	-21.13	PN/A	1,208	1,148	-17.13	-17.32	1,494	1,280
10/29/00 09:30:00	1949.2	200.5	484,123	2,799	0.48	0.00	0.64	1948	-12.88	48	160	715	714	-27.78	1088	1,072	-20.78	PN/A	1,204	1,149	-18.78	-17.02	1,494	1,280
10/29/00 09:35:00	1950.2	203.4	484,329	2,800	0.48	0.00	0.42	2098	-13.81	48	163	718	717	-27.78	1087	1,073	-20.90	PN/A	1,208	1,150	-18.74	-17.84	1,493	1,284
10/29/00 09:40:00	1951.2	200.6	484,532	2,801	0.18	0.04	0.28	2017	-12.87	48	164	720	720	-27.87	1078	1,081	-20.18	PN/A	1,211	1,154	-18.58	-18.80	1,494	1,242
10/29/00 09:45:00	1952.2	200.6	484,733	2,802	1.02	17.14	0.28	2098	-12.87	48	168	723	724	-27.18	1074	1,079	-19.87	PN/A	1,209	1,155	-18.34	-18.83	1,491	1,219
10/29/00 09:50:00	1953.2	188.3	484,933	2,803	0.00	18.18	0.88	2088	-11.88	48	161	726	731	-34.71	1088	1,088	-18.89	PN/A	1,212	1,187	-14.71	-18.88	1,491	1,278
10/29/00 09:55:00	1954.2	188.4	485,130	2,804	0.08	18.88	0.88	2108	-18.88	48	161	729	733	-22.88	1082	1,088	-18.88	PN/A	1,214	1,158	-13.48	-18.84	1,491	1,231
10/29/00 09:58:00	1956.2		485,288	2,805																				
10/29/00 09:59:00	1956.2	200.2	4,883	34.1	0.77	2.17	0.89	2088	-12.18	43	173	712	712	-28.84	1083	1,070	-18.84		1,201	1,148	-18.47	-18.88	1,492	1,253
10/29/00 10:00:00	1956.2	200.2	4,883	34.1	0.78	2.21	0.87	2071	-12.18	43	173	712	712	-28.87	1083	1,070	-18.83		1,201	1,148	-18.48	-18.88	1,492	1,253

11/30/2000 14:32 3852284375 CSR RINKER PAGE 02

EQUIPMENT CALIBRATIONS

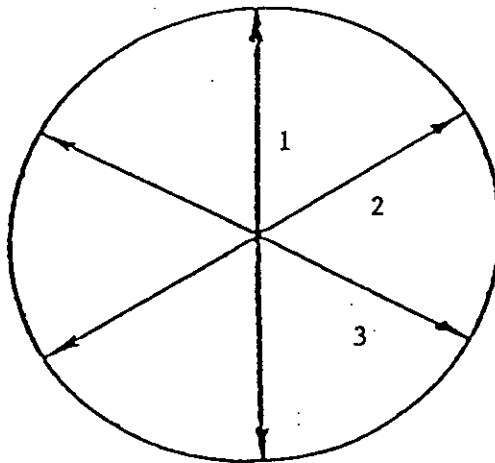
NOZZLE CALIBRATION

DATE 9-29-00
PLANT NAME Rinker
LOCATION Miami
SOURCE Cement Kiln

<u>Measurement No.</u>	<u>Inside Diameter (inches)</u>
<u>1</u>	<u>0.255</u>
<u>2</u>	<u>0.253</u>
<u>3</u>	<u>0.254</u>

Average 0.254
Area of Nozzle 0.0003519 ft²

Calibrated by: R Paul



Nozzle X-Section



PITOT TUBE CALIBRATION MEASUREMENTS

PITOT TUBE IDENTIFICATION NO. SS III

DATE CALIBRATED 8-14-98

PITOT TUBE ASSEMBLY LEVEL ? X YES _____ NO

PITOT TUBE OPENINGS DAMAGED ? _____ YES (EXPLAIN BELOW) _____ NO

$\alpha_1 =$ 3.0 $^\circ$ ($<10^\circ$) $\alpha_2 =$ 3.0 $^\circ$ ($<10^\circ$)

$\beta_1 =$ 0.0 $^\circ$ ($<5^\circ$) $\beta_2 =$ 1.5 $^\circ$ ($<5^\circ$)

$\gamma =$ 0.0 $^\circ$, $\theta =$ 1.0 $^\circ$, $A =$ 0.970 IN. = (PA+PB)

$Z = A \sin \gamma =$ 0.0 IN. (<0.125 IN.)

$W = A \sin \theta =$ 0.0169 IN. (<0.031 IN.)

$P_A =$ 0.501 IN. $P_B =$ 0.470 IN.

$D_t =$ 0.375 IN. (≥ 0.1875 IN. ≤ 0.3750 IN.)

COMMENTS: Pitot tubes looked OK day of test

CALIBRATION REQUIRED? _____ YES X _____ NO

CALIBRATED BY: R Paul

PTCMFORM 1/8/87

POST TEST THERMOCOUPLE
CALIBRATION

DATE 9-29-00

PLANT NAME Reiber Cement

LOCATION Miami, FL

SOURCE Cement Kiln

Thermocouple Readout # KA-2

Umbilical Cord # 100'

Switch Box # KA-2

Thermocouple # KA-38

Average Stack Temperature °F 291

*Observed Mercury in Glass (ASTM) °F 244

Observed Thermocouple Reading °F 246

Percent Difference $\frac{(ASTM + 460) - (Thermo + 460)}{(ASTM + 460)} \times 100 = 0.28\%$

Tolerance $\leq 1.5\%$

* Observed Temperature must be within ten percent of the average stack temperature.

RPaul
Signature



KOGLER & ASSOCIATES, ENVIRONMENTAL SERVICES
 ANNUAL THERMOCOUPLE CALIBRATION 12/27/99

KA70 RO/UMB		ICE (F)	ASTM (F)	AMB. (F)	ASTM (F)	212 (F)	ASTM (F)	400 (F)	ASTM (F)	KA70 RO/UMB		
KA1/100'	STACK	32	33	73	72	208	209	405	406	KA1/100'	STACK	
	BOX	33	32	72	72	210	210	404	406		BOX	
	IMP	32	32	73	73	211	212	400	401		IMP	
KA2/200'	STACK	33	33	73	72	209	210	415	416	KA2/200'	STACK	
	BOX	32	32	72	73	211	210	418	418		BOX	
	IMP	32	33	71	72	212	212	409	410		IMP	
KA3/25' SWBXXA3	STACK	32	33	73	73	211	210	409	410	KA3/25'	STACK	
	BOX	33	32	72	73	215	215	415	416		BOX	
	IMP	33	32	72	73	212	212	408	407		IMP	
KA4/25' SWBXXA3	STACK	32	32	73	74	205	205	420	420	KA4/25'	STACK	
	BOX	32	33	74	74	207	208	422	421		BOX	
	IMP	32	33	72	73	211	212	425	425		IMP	
KAK/200K KAK-38 SWBXXAK1	STACK	31	32	74	74	213	213	419	420	KAK/200K	STACK	
	BOX	32	32	72	73	215	216	422	422		KAK-38	BOX
	IMP	32	33	74	73	219	220	400	401		IMP	
KA1/200'	STACK	33	33	73	73	211	210	422	422	KA1/200'	STACK	
	BOX	33	33	73	72	214	214	419	418		BOX	
	IMP	33	32	73	72	209	209	425	425		IMP	
KA2/100'	STACK	33	33	73	72	209	210	422	423	KA2/100'	STACK	
	BOX	33	32	73	74	212	211	425	425		BOX	
	IMP	32	33	72	73	212	211	426	425		IMP	

Signature *[Handwritten Signature]*

Date 12/27/99

KOUGLER & ASSOCIATES, ENVIRONMENTAL SERVICES
 ANNUAL THERMOCOUPLE CALIBRATION 12/27/99

THERMOCOUPLE #	ICE (F)	ASTM (F)	AMB. (F)	ASTM (F)	212 (F)	ASTM (F)	400 (F)	ASTM (F)	THERMOCOUPLE #
KA-06	33	33	73	74	212	212	420	419	KA-06
KA-07	33	32	74	75	209	210	421	422	KA-07
KA-08	34	33	74	74	211	211	415	416	KA-08
KA-09	33	33	74	74	215	216	416	417	KA-09
KA-10	34	33	72	72	214	215	408	407	KA-10
KA-11	33	33	72	72	212	212	415	414	KA-11
KA-12	33	33	73	72	219	220	408	407	KA-12
KA-38	34	33	73	74	211	211	412	411	KA-38
KA-39	34	33	73	73	212	211	416	415	KA-39
KA-50	33	34	74	73	215	214	415	416	KA-50
KA-64	33	33	74	74	211	211	410	411	KA-64
KA-70	33	33	73	74	212	213	405	406	KA-70
KA-71	34	34	73	73	211	210	407	408	KA-71
KA-72	34	33	72	72	216	215	410	410	KA-72
KA-105	34	33	73	73	217	218	404	405	KA-105
KA-108	34	34	72	73	214	215	412	411	KA-108
KA-115	34	33	72	72	213	214	409	410	KA-115
KA-126	34	33	72	72	216	216	410	409	KA-126

THERMOCOUPLE #	ICE (F)	ASTM (F)	AMB. (F)	ASTM (F)	212 (F)	ASTM (F)	400 (F)	ASTM (F)	THERMOCOUPLE #
KAK-08	32	32	73	74	218	217	407	406	KAK-08
KAK-09	31	31	73	73	211	212	405	406	KAK-09
KAK-10	32	32	74	74	209	210	377	376	KAK-10
KAK-11	31	31	75	75	206	206	399	398	KAK-11
KAK-12	32	31	74	74	218	217	407	406	KAK-12
KAK-38	31	31	74	74	210	211	410	410	KAK-38
KAK-65	32	32	74	74	205	205	377	377	KAK-65
KAK-72	31	31	74	75	208	208	400	401	KAK-72
KAK-110	31	32	75	74	209	210	399	400	KAK-110
KAK-07	32	31	75	74	209	210	389	390	KAK-07

VOST SWITCH BOX	T. COUPLE				
CH#1	C-1	32	33	74	75
CH#2	C-1	33	32	74	74
CH#3	C-1	33	33	75	74

VOST SWITCH BOX					
CH#1	C-2	32	33	73	74
CH#2	C-2	33	33	74	75
CH#3	C-2	32	33	75	75

Signature Steph J. Bee
 Date 12/27/99

KOGLER & ASSOCIATES, ENVIRONMENTAL SERVICES
 ANNUAL THERMOCOUPLE CALIBRATION 12/27/99

Range (°C)	Measured Voltage (mV)	Measured Voltage (V)	Calc. Temp. (°C)	Readout Temp. (°C)	Percent Difference (%)
KAK-12	28.7	0.029	690	693	-0.45023
	37.4	0.037	902	900	0.217654
KAK-38	28.9	0.029	694	698	-0.51192
	37.2	0.037	897	900	-0.33898
KAK-72	28.5	0.029	685	687	-0.30387
	37.5	0.038	904	908	-0.39058
KAK-65	28.2	0.028	678	680	-0.32666
	37.8	0.038	912	910	0.218082
KA-110	29	0.029	694	699	-0.65592
	37	0.037	894	899	-0.50758

EQUATIONS :

$$T(\text{calc.}) = (0.226584602 + (24152.109 * V) + (67233.4248 * V^2) + (2210340.682 * V^3) - (860963914.9 * V^4) + (48350600000 * V^5) - (1184520000000 * V^6) + (13869000000000 * V^7) - (63370800000000 * V^8))$$

Where :

V = Measured Voltage (Volts)

T(calc.) = Temperature calculated based on voltage

Signature Steph S Bee

Date 12/27/99

POST-TEST DRY GAS METER CALIBRATION FORM

COMPANY: RINKER / MIAMI, FL.
 SOURCE: CEMENT KILN
 DATE: SEPT. 29 2000
 PRETEST Y: 1.000
 TEST METER NUMBER: KA.1
 METER BOX NUMBER: KA.2
 BAROMETRIC PRESSURE (Pb): 30.11
 DELTA H (dH): 1.7

	TEST METER READING (ft ³)	DRY GAS READING (ft ³)	TIME (min) \pm	VACUUM SETTING (in. Hg)
INITIAL	636.282	152.563		
FIRST	642.680	158.941	8	6
SECOND	650.692	166.969	10	6
THIRD	657.888	174.162	9	6

DELTA H	TEST METER Vt (ft ³)	DRY GAS Vd (ft ³)	TEST METER TEMP. Tt (F)	DRY GAS TEMP. Td (F)
1.7	6.398	6.378	78	85
PB	8.012	8.028	78	87
30.11	7.196	7.193	78	88

	Yi	$Vt * Pb * (Td + 460)$	$Vd * (Pb + dH / 13.6) * (Tt + 460)$
RUN 1 (Yi)=	1.011986	104990.8	103747.2
RUN 2 (Yi)=	1.010507	131959.0	130586.9
RUN 3 (Yi)=	1.014799	118736.0	117004.4
AVG. Y =	1.012431		

PRETEST Y = 1.000
 AVG. DELTA Y = 0.012431
 DELTA Y LIMIT = 0.05
 IS TEST WITHIN 5%? YES

- Vt = Gas volume passing through the test meter, ft³
- Vd = Gas volume passing through the dry gas meter, ft³
- Tt = Temperature of the gas in the test meter, |F
- Tdi = Temperature of the inlet gas of the dry gas meter, |F
- Tdo = Temperature of the outlet gas of the dry gas meter, |F
- Td = Average temperature of the gas in the dry gas meter, the average of Tdi and Tdo, |F
- dH = Pressure difference across the orifice, in, H2O
- Yi = Ratio of test meter to dry gas meter for each run
- Y = Average ratio of accuracy of test meter to dry gas meter for all three runs, tolerance = pretest * 0.05 * Y
- \pm = Time of calibration run, min
- Pb = Barometric pressure, in Hg.

DRY GAS METER AND ORIFICE CALIBRATION

CONTROL BOX NO. KA.2 BAROMETRIC PRESS. 30.03 IN. HG.
 DATE AUGUST 25, 2000 PERFORMED BY ROC

	RUN 1	RUN 2	RUN 3	RUN 4	RUN 5
VACUUM ("Hg)	0.0	0.0	0.0	0.0	0.0
dHw ("H2O)	-0.22	-0.23	-0.24	-0.30	-0.32
dHd ("H2O)	0.50	1.00	1.50	2.50	3.50
INITIAL WTM	511.428	540.800	501.618	549.333	519.067
FINAL WTM	519.067	548.912	511.159	561.876	532.626
INITIAL DGM	29.303	59.064	19.500	67.710	36.982
FINAL DGM	36.982	67.289	29.040	80.382	50.782
TEMP. WTM (F)	76.00	76.00	76.00	76.00	76.00
TEMP. DGM (F)	82.00	80.00	79.50	80.00	94.00
TEST TIME (MIN.)	17.50	13.50	13.00	13.00	12.00

NET VOLUME WTM	7.639	8.112	9.541	12.543	13.559
NET VOLUME DGM	7.679	8.225	9.540	12.672	13.800
Y	1.005	0.992	1.004	0.992	1.008
dH@	1.468	1.555	1.565	1.508	1.501

AVERAGE Y = 1.000

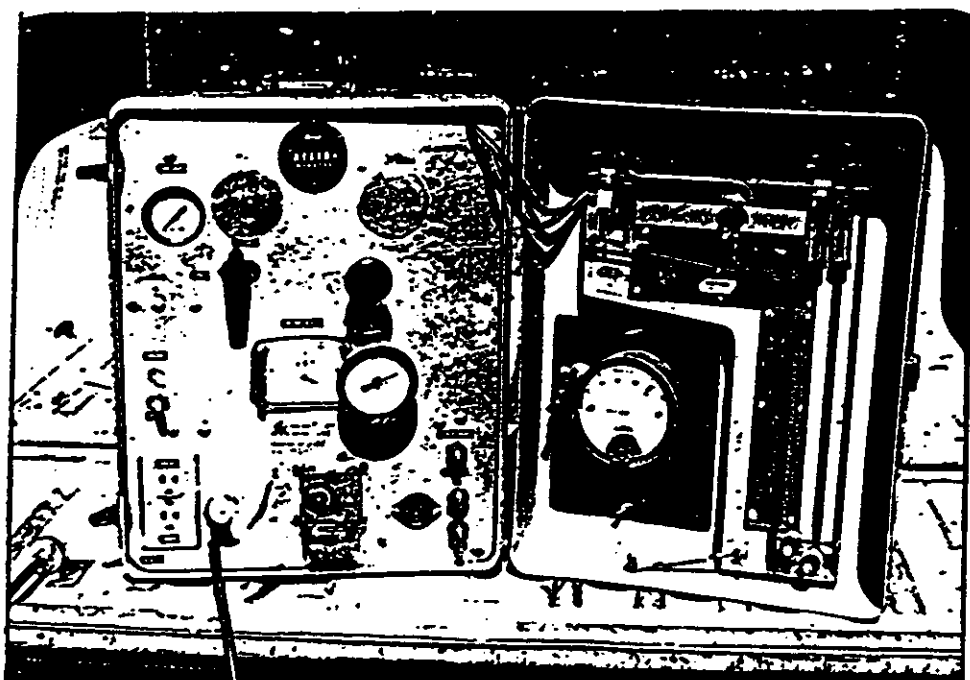
ACCEPTABLE Y RANGE = 0.980 TO 1.020 OK

AVERAGE dH@ = 1.520

$$Y = \frac{V_w (P_b - (dH_w / 13.6)) \times (T_d + 460)}{(T_w + 460)} \div \frac{V_d (P_b + (dH_d / 13.6)) \times (T_d + 460)}{(T_w + 460)}$$

$$dH@ = 0.0317 \times dH_d / (P_b (T_d + 460)) \times ((T_w + 460) \times \text{time}) / V_w^2$$

SOURCE SAMPLING EQUIPMENT



METER BOX

Equipment used in Source Sampling is either manufactured by or assembled by Koogler & Associates. The guidelines followed are A.P.T.D. 0581, Details of Isokinetic Source Sampling Equipment and A.P.T.D. 0576, Maintenance, Calibration and Operation of Isokinetic Source Sampling Equipment.

PROJECT PARTICIPANTS



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