

EXHIBITS 1 - 17

RESPONSE OF OGDEN MARTIN SYSTEMS OF LAKE, INC.

TO

FLORIDA DEPARTMENT OF ENVIRONMENTAL PROTECTION

WARNING LETTER OWL-AP-99-413

SUBMITTED JULY 15, 1999

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July 15, 1999

VIA U.P.S. NEXT DAY AIR

Vivian F. Garfein
Director of District Management
Central District
Florida Department of Environmental Protection
3319 Maguire Boulevard, Suite 232
Orlando, FL 32803-3767

Re: Warning Letter OWL-AP-99-413

Dear Ms. Garfein:

By this letter and accompanying document submission, Ogden Martin Systems of Lake, Inc. ("OMSL" or "the Company") provides its response to the referenced Warning Letter, which was issued by the Florida Department of Environmental Protection, Central District ("DEP" or "the Department") on June 15, 1999, and received by Dr. Gary K. Crane on behalf of OMSL on June 18, 1999. The Warning Letter states that OMSL's response thereto is due "within 15 days of receipt" of same, or July 3, 1999; however, the deadline for OMSL's response since has been extended by the Department until July 16, 1999. A copy of OMSL's letter to DEP memorializing this extension, as well as OMSL's request for a meeting with the Department to discuss the issues raised in the Warning Letter, is attached as Exhibit 1.

EXECUTIVE SUMMARY

The Warning Letter raises numerous factual and legal issues that the Department contends are evidence that OMSL's operations have resulted in violations of applicable environmental statutes, regulations and permit requirements. Nothing could be farther from the truth.

OMSL, as a good environmental citizen, has always endeavored to work cooperatively and openly with the Department, as demonstrated by the circumstances underlying the Warning Letter. It thus should be understandable that the Warning Letter

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comes to OMSL as an unpleasant surprise. As discussed in further detail below, the specific mercury emissions stack tests cited as evidence of alleged noncompliance were conducted by OMSL in the presence of DEP officials using pre-approved protocols, and the test results were timely and fully reported to the Department. OMSL in good faith worked closely with DEP to resolve the issues of concern raised by the tests in a timely, compliant and cooperative manner, and OMSL believed that all issues had, in fact, been resolved satisfactorily. Indeed, through its own initiative, OMSL discovered and reported to DEP that illegal mercury contamination of the municipal wastestream entering the Facility was occurring – contamination which, as it turns out, was the result of a hazardous waste site cleanup in Lake County known to and overseen by DEP. Certainly, had DEP informed OMSL of this cleanup plan, OMSL would have objected to the shipment of mercury-contaminated waste materials to the Facility. With respect to biohazardous waste, OMSL has at all times kept DEP fully apprised of the Facility's operations. If the Department seriously believed that OMSL somehow was processing biohazardous waste improperly, there was no need for a 15-plus month delay in raising the issues of concern for resolution.

Turning to the specific issues raised by the Department in the Warning Letter, OMSL contends that the results of mercury emissions stack testing in January 1998 do not evidence noncompliance, nor do they evidence any technological or operational problems at the Facility. Rather, the January 1998 mercury stack test results were mutually understood by OMSL and DEP at the time of the events in question as anomalous and not as evidence of non-compliance. Following discussions with the Department, a re-test was scheduled for April 1998 for purposes of satisfying the annual compliance demonstration requirement with respect to mercury emissions. That re-test demonstrated compliance. Additional testing undertaken in March 1998 also evidenced compliance and further supports the conclusion that the January 1998 stack test results were anomalous. In sum, the facts belie the Department's assertions that the January 1998 stack test results are evidence of noncompliance, and that OMSL failed to properly document those results or take appropriate corrective action.

OMSL successfully demonstrated annual compliance with mercury emission limits in April 1998 for both Units 1 and 2. By agreement with DEP, the April 1998 stack testing was conducted for the dual purpose of demonstrating compliance with mercury emission limits and to demonstrate that Unit 2 is capable of meeting applicable emissions limits – including but not limited to the mercury emissions limit – while co-burning biohazardous waste and municipal solid waste. The Department's assertion in the Warning Letter that the April 1998 testing of Unit 1 resulted in a de facto "derate" of the Unit with respect to the processing rate for biohazardous waste is not supported in law and is demonstrably incorrect on the facts, which demonstrate that Unit 1 is and has been capable of processing biohazardous waste at the full permitted rate of 2.15 tons/hr.

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DEP's suggestion that the Unit 2 testing was not conducted in a manner sufficient to demonstrate compliance with mercury emissions limits likewise is in error.

The unprecedented inlet concentrations of mercury and poor removal efficiencies achieved during the Facility's January 1999 mercury compliance stack tests do not evidence noncompliance as alleged in the Warning Letter, nor do they evidence any technological or operational problems at the Facility. Instead, the direct and proximate cause of those stack test results was illegal contamination of the municipal wastestream with mercury materials – including broken mercury thermometers, soil and debris – from a hazardous waste cleanup site in Lake County. The source of the mercury contamination was unknown to OMSL at the time of the January 1999 stack tests, but was later discovered by OMSL and reported to DEP. OMSL since has learned that DEP not only knew of this source prior to the January 1999 stack test, but had in fact approved a site cleanup plan in 1995 allowing mercury-contaminated wastes to be sent to the Facility for destruction. Under these circumstances, it is plainly inequitable for the Department to bring an enforcement action against OMSL with respect to the January 1999 mercury stack test results. OMSL also rejects the Department's suggestion that the January 1999 mercury stack test report did not include all required data.

OMSL demonstrated annual compliance with mercury emissions limits in April 1999 (Unit 1) and June 1999 (Unit 2). These results support OMSL's view that, but for the illegal wastestream contamination with mercury that occurred in January 1999, the Facility would have successfully demonstrated compliance at that time. Additional investigations undertaken by OMSL prior to and during the April 1999 stack tests also demonstrate that the January 1999 stack test results were not attributable to any technological or operational problems at the Facility.

OMSL is not permitted to burn, and does not burn, materials that are subject to regulation as hazardous wastes. The Department's allegation in the Warning Letter that OMSL accepted and processed "hazardous" chemotherapy waste in January 1999 previously has been demonstrated to DEP officials as being incorrect.

OMSL is and has been in compliance with all applicable carbon injection rate requirements, including recordkeeping requirements. The Department's suggestion in the Warning Letter that OMSL's recordkeeping with respect to the rate at which carbon is injected into the air pollution control system for mercury emissions control thus is in error.

Finally, and perhaps most importantly, there exists no evidence to suggest that OMSL is operating or has operated the Facility in a manner that presents a threat to human health or the environment. OMSL is committed to conducting its business

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operations in a manner that is both compliant with law and protective of Florida's environment and the health and welfare of the Facility's workers and the community at large. OMSL is confident that, when all of the facts are presented in light of applicable law, it will be shown that no enforcement action against the Facility is warranted.

OMSL's detailed response to the Department's factual and legal allegations is as set forth below.¹

DISCUSSION

I. ISSUES PERTAINING TO STACK TESTING, 1998 - 1999

A. Regarding Tests Conducted January 27 Through January 29, 1998

During the time period from January 27 - 29, 1998, OMSL conducted stack tests on both Units 1 and 2 of the Lake County Resource Recovery Facility ("Facility") to demonstrate, among other things, compliance with applicable mercury emission limits. These tests were undertaken in accordance with Source Test Plan - OEG Report No. 2193, dated December 2, 1997, which previously had been submitted to the Department for review. Mr. Garry Kuberski of DEP's Central District was present during the conduct of the stack tests.

A total of six (6) sample runs were conducted, or three (3) runs per Unit. The carbon injection rate to the air pollution control system during the stack test was 11.2 pounds per hour ("lb/hr") per Unit. This was the same carbon injection rate used successfully at the Facility since July 1, 1995, when OMSL began to use carbon injection for mercury emissions control per Rule 62-296.416, F.A.C.

The preliminary sampling results were received by OMSL from the testing laboratory in late February. OMSL was surprised to learn that two of the six samples indicated higher outlet than inlet concentrations of mercury. On February 29, 1998,

¹ OMSL has made every effort to provide a full and complete response to the DEP's allegations, as OMSL understands them. The Warning Letter, however, includes many legal citations that are not tied specifically to supporting factual allegations. OMSL hereby reserves the right to respond to any and all factual or legal assertions that the Department may purport to have included in the Warning Letter, but which were not reasonably identifiable by OMSL on the face of that document. In addition, issues or questions may arise at our upcoming meeting that are not addressed specifically in this response. OMSL reserves the right to supplement this response as necessary to address any such additional issues as well.

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OMSL's Jason Gorrie telephoned Dr. Anatoliy Sobolevskiy of DEP's Central District to provide a preliminary verbal report of the test results, including the apparent "negative removal" phenomenon that had occurred with respect to two of the mercury samples.

By letter dated March 11, 1998, the final report for the January 1998 stack tests was submitted to the Department through Dr. Sobolevskiy (see Environmental Test Report – OEG Report No. 2252, dated March 6, 1998). The March 11, 1998 cover letter accompanying that report states that:

The mercury results for Units 1 and 2 were not consistent with the results expected for systems with carbon injection. These results, as discussed with you by Jason Gorrie on February 29, 1998, do not seem possible with carbon injection systems for mercury control. We can discuss these results with you after your review of the test report.

A copy of the March 11, 1998 letter is attached as Exhibit 2.

OMSL's Environmental Test Report, Volume 1, Executive Summary, at page 1, also characterized the conduct and results of the mercury sampling, as follows:

The mercury emission data for both units are not consistent with the control efficiency expected with activated carbon injection systems. The carbon injection system at the facility operated in accordance with permit requirements at all times without malfunction. The laboratory analysis for mercury was conducted twice.

A copy of Volume 1 of the Environmental Test Report is attached as Exhibit 3.

On March 30, 1998, OMSL representatives Jason Gorrie, Cecil Boatright, Gary Main and Joe Aldina held a conference call with DEP's Anatoliy Sobolevskiy. The purpose of this call was to discuss the January 1998 stack test results. OMSL was advised by Dr. Sobolevskiy that DEP had reviewed the test results, and that, in the view of himself and others within the Department, the only apparent explanation for the "negative removal" phenomenon with respect to mercury was sampling error and/or sample contamination.

Based on that March 30 telephone conversation, OMSL understood that the Department had not determined that the Facility was out of compliance with mercury emissions standards, but instead was taking the position that the Facility had yet to make the required annual compliance demonstration. Dr. Sobolevskiy informed OMSL that a re-test for purposes of making the annual mercury compliance demonstration should be undertaken as soon as possible. Several dates in June 1998 were discussed owing to the

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Facility's outage schedule; however, Dr. Sobolevskiy required that the testing be undertaken in April 1998.

OMSL's understanding that a re-test to demonstrate compliance with mercury emissions limits had been agreed to by the Department as the appropriate course of action in light of the anomalous January 1998 stack test results is further demonstrated by a June 2, 1998 letter from OMSL's Jason Gorrie to Mr. Leonard Kozlov, P.E., of DEP's Central Office. That letter, which accompanied the submission of the results of the April 1998 stack tests, states, in pertinent part:

As you are aware, the results from mercury stack testing in January indicated likely sample contamination. As a result, and following discussions with Dr. Anatoliy Sobolevskiy of your staff, a re-test was undertaken in order to demonstrate compliance with the mercury emission limiting standard found at 62-296.413 [sic], F.A.C.

A copy of the June 2, 1998 letter is attached as Exhibit 4.

In light of the above-referenced conversations with DEP, and as discussed in further detail below, OMSL scheduled another mercury compliance stack test for April 20 - 23, 1998. Under all the circumstances, OMSL believed that the re-test was the only reasonable and necessary "corrective action." The January 1998 mercury test results had been attributed by the Department and OMSL to sampling problems independent of the operation of the Facility. As the Department is aware, the April 1998 stack tests demonstrated compliance with applicable mercury emission limits.

OMSL notes as well that, during the period of time between the January 1998 and April 1998 compliance tests, a number of additional tests were run on Units 1 and 2, both of which provide evidence that the Units were in compliance with applicable mercury emission limits. Specifically, a test program to evaluate Units 1 and 2 for mercury speciation and performance was run March 3 and 4, 1998. Unit 1 demonstrated compliance with an average mercury removal efficiency of 91.7% (average mercury outlet concentration was 81.6 ug/dscm @ 7% O₂); Unit 2 averaged 94.5% removal efficiency (average mercury outlet concentration was 6.6 ug/dscm @ 7% O₂).

A follow-up mercury emissions test program was done on March 19 and 20, 1998, and both Units again provide evidence of compliance. The average mercury outlet concentration for Unit 1 (for seven (7) test runs) was 30.2 ug/dscm @ 7% O₂, with an average removal efficiency of 70.4%. The average mercury outlet concentration for Unit 2 (for two (2) test runs) was 13.9 ug/dscm @ 7% O₂, with an average removal efficiency of 91.6%. All of the March 1998 tests were run at compliance test conditions for steam

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load and medical waste throughput on Unit 1. The carbon system was calibrated before each test run and at the end of the test day. Copies of the reports for the March 1998 test reports are provided as Exhibits 5 and 6.²

For the foregoing reasons, OMSL takes issue with the statement on page 1 of the Warning Letter that “the file indicates that the company suspected that the samples were contaminated, but no supporting written information or other corrective action information was provided other than the stack test.” As outlined above, OMSL informed the Department both in writing and orally that the mercury removal efficiencies determined during stack testing were not consistent with the control efficiencies expected using carbon injection, and also were not attributable to a malfunction of the carbon system. Thus, DEP’s suggestion that OMSL violated Section 403.161(1)(b), F.S. and Permit AO35-193817 by not providing *additional* information or documentation about the January 1998 stack test lacks merit. Although, in hindsight, DEP might wish to see additional information in the file with respect to that event, the fact remains that contemporaneous written and oral reports were provided to the Department and no request was ever made by Department representatives for additional information.

Additionally, OMSL disagrees with DEP’s suggestion, at pages 1 – 2 of the Warning Letter, that the January 1998 mercury stack test results establish a violation of Rule 62-296.416, F.A.C. and Permit AC35-264176. While OMSL does not dispute that the mercury stack test results, if valid, were in excess of applicable mercury emission limits, it was apparent at the time that Department representatives concurred with OMSL’s view that the most prudent course of action was to re-test, insofar as the January 1998 sampling results appeared invalid. Under all of the circumstances, it was OMSL’s understanding that the January 1998 results were to be considered a nullity and that the April 1998 stack tests instead would serve as the annual compliance demonstration required by Rule 62-296.416, F.A.C. The successful April 1998 re-test corroborated OMSL’s conclusion that the mercury results obtained in January 1998 were most likely attributable to sampling error or sample contamination, and do not evidence any technological or operational problems at the Facility. Indeed, available data and information from both March 1998 test programs demonstrate that the January 1998 stack test was an anomaly, and that the Facility was operating within prescribed mercury emission limits well before the successful April 1998 re-test. Accordingly, no violation(s) should be deemed to exist as a result of the January 1998 stack tests.

² Engineering Test Report, Units 1 and 2, dated April 21, 1998 (test dates March 3 – 4, 1998) (AirKinetics, Inc.); Engineering Test Report, Units 1 and 2, dated April 22, 1998 (test dates March 19 – 20, 1998) (AirKinetics, Inc.).

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B. Regarding Tests Conducted April 20 Through 23, 1998

In the wake of the January 1998 stack testing discussed above, OMSL scheduled another series of stack tests for April 20 – 23, 1998. These stack tests were intended to serve a dual purpose: (1) to demonstrate compliance with applicable mercury emission limits; and (2) to obtain data necessary to support a permit modification allowing for the combustion of biohazardous waste in Unit 2. As the Central District is aware, testing of Unit 2 while burning biohazardous waste was undertaken by agreement with the Bureau of Air Regulation in Tallahassee.³

The stack tests were undertaken in accordance with Source Test Plan – OEG Report No. 2256, dated April 6, 1998, which previously had been submitted to the Department for review. The Source Test Plan, which was approved by DEP, states at page 1 that “[b]iohazardous waste will be charged to Unit 1 and Unit 2 during testing.” The Source Test Plan also demonstrates clearly and unambiguously that OMSL’s plan was to test Unit 1 for mercury emissions compliance only, while at the same time testing Unit 2 for compliance with mercury emissions limits as well as all other parameters necessary to support a permit application to burn biohazardous waste in that Unit. A copy of the Source Test Plan for the April 1998 stack testing is attached as Exhibit 7.

The stack testing was conducted as scheduled and per the approved Source Test Plan. Messrs. Garry Kuberski and Anatoliy Sobolevskiy of DEP’s Central District were present during the conduct of the stack tests. As was the case in January 1998, the carbon injection rate to the air pollution control system during the stack testing was 11.2 lb/hr per Unit. A total of six (6) sample runs were conducted for purposes of analysis of mercury emissions, or three (3) runs per Unit. By letter dated June 2, 1998, the final reports for the April 1998 mercury compliance stack tests was submitted to the Department through Mr. Leonard Kozlov (see Environmental Test Report – OEG Report No. 2252, dated March 6, 1998). As further detailed in that Environmental Test Report, both Unit 1 and Unit 2 demonstrated compliance with applicable mercury emissions limits as required by Rule 62-296.416, F.A.C. and Permit AC35-264176.

Additional information pertinent to the April 1998 stack tests, specifically, the biohazardous waste throughput rates for each Unit in tons per hour (tons/hr), was resubmitted in summary form by OMSL to the Department by letter dated July 7, 1998 from Jason Gorrie to Garry Kuberski. That July 7, 1998 letter states that the

³ OMSL contends that both Units at the Facility are permitted to burn biohazardous waste per Permit AC35-115379 (PSD-FL-113). With the exception of the April 1998 stack testing, however, OMSL has not burned biohazardous waste in Unit 2. OMSL currently has pending before the Department an application to revise Permit AC35-115379 that would, among other things, establish a biohazardous waste processing limit for Unit 2.

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biohazardous waste feed rate during the conduct of the stack tests averaged 1.12 tons/hr for Unit 1, and 2.02 tons/hr for Unit 2. The permitted biohazardous waste feed rate for Unit 1 is 2.15 tons/hr.

The compliance test runs for Unit 2 were conducted on April 21 at a biohazardous waste rate approximating the permitted rate for Unit 1. As a result, by the time that the Unit 1 compliance tests were run on April 23, the supply of biohazardous waste on-site had been reduced, and a scheduled delivery of such waste that would have replenished the supply failed to arrive. Thus, Unit 1 was charged at a lower total biohazardous waste feed rate during testing than was Unit 2. DEP Central District representatives were on-site during the stack tests, were aware of the biohazardous waste supply situation, and advised OMSL to continue with the testing of Unit 1 at the unavoidably lower biohazardous waste feed rate. The Unit was charged continuously with biohazardous waste during the test program.⁴

1. Unit 1

With the foregoing as background, OMSL strongly disagrees with the position asserted by the Department at page 2 of the Warning Letter that, "Unit 1 . . . should have been de-rated from 2.15 tons of medical waste to 1.2 tons per hour of medical waste" as a consequence of the April 1998 stack tests, which the Department concedes were a "successful[] re-test[]" for mercury emissions compliance. Although not clearly articulated in the Warning Letter, it appears that the Department is of the view that that Rule 62-297.310(2), F.A.C., stands for the proposition that emissions units must be tested at 90 to 100 percent of the permitted capacity *for each waste type fed to the unit*. Building on the position, the Department evidently believes that Unit 1 should have been de-rated with respect to biohazardous waste throughput from the permit level of 2.15 tons/hr to approximately 1.2 tons/hr, the latter being 110 percent of the average biohazardous waste throughput to Unit 1 during the compliance tests.

OMSL disagrees with the Department's reading of Rule 62-297.310(2), F.A.C., which finds no support in the reported administrative or judicial decisions. The Rule provides that:

⁴ As previously discussed, the retest was conducted in April at the direction of DEP, rather than in June as was preferred by OMSL for operational reasons (*i.e.*, the Facility outage schedule). This acceleration of the retest schedule did not allow OMSL sufficient time to accumulate biohazardous waste on-site prior to the testing. As a result, by the time that the Unit 1 testing was conducted, there was not enough biohazardous waste on-site to run Unit 1 at the full permitted capacity for that waste type.

(2) Operating Rate During Testing. Unless otherwise stated in the applicable emission limiting standard rule, testing of emissions shall be conducted with the emissions unit operation at permitted capacity as defined below. If it is impracticable to test at permitted capacity, an emissions unit may be tested at less than the minimum permitted capacity; in this case, subsequent emissions unit operation is limited to 110 percent of the test rate until a new test is conducted. Once the unit is so limited, operation at higher capacities is allowed for no more than 15 consecutive days for the purpose of additional compliance testing to regain the authority to operate at the permitted capacity.

* * *

(b) All Other Sources. Permitted capacity is defined as 90 to 100 percent of the maximum operation rate allowed by the permit.

As is clear from the face of the Rule, all that is required to demonstrate compliance with the operating rate requirement during stack testing is that the Unit in question be operated at "90 to 100 percent of the maximum operation rate allowed by the permit." Contrary to the Department's suggestion, the Rule does not subcategorize the "permitted operating rate" by fuel type. The Rule instead concerns itself with the need for compliance tests to be conducted when emissions units are at or near their permitted capacity, presumably to avoid "circumvention" of applicable emissions limits by means of operating the emissions unit at an artificially low capacity during the compliance test. OMSL notes that the Facility's permits likewise do not establish a requirement that stack testing of Unit 1 be conducted while burning biohazardous waste at a rate equal to 90 to 100 percent of the permitted 2.15 tons/hr maximum rate.

During the April 1998 compliance tests, OMSL operated Unit 1 at ≥ 90 percent of the Unit's permitted steam flow capacity, which accounts for all waste types, including both municipal solid waste and biohazardous waste. Thus, OMSL demonstrated compliance with Rule 62-297.310(2), F.A.C. Although OMSL operated Unit 1 at a biohazardous waste feed rate less than 90 to 100 percent of the Unit's permitted capacity for that subcategory of waste, as discussed above, the Rule does not require that each type of waste to the Unit be the subject of a separate compliance test. Nor did OMSL circumvent the intent of the Rule; the Unit was operated at a capacity level sufficient to demonstrate that the Unit is capable of meeting applicable mercury emissions limits when operating at full load. Thus, no violation of Rule 62-297.310(2), F.A.C. exists, and OMSL cannot be held to have exceeded the alleged de facto "de-rated" biohazardous waste throughput rate of 1.2 tons/hr in the wake of the April 1998 compliance test.

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Furthermore, even assuming for the sake of argument that the Department is correct in its assertion that Rule 62-297.310(2), F.A.C. required OMSL to operate Unit 1 at 90 to 100 percent of the Unit's permitted capacity for biohazardous waste in order to avoid "de-rating" the Unit with respect to that waste type, ample evidence exists to demonstrate that Unit 1 is and was capable of burning biohazardous waste at the permitted throughput rate of 2.15 tons/hr while maintaining compliance with applicable mercury limits. As the Department is aware, compliance tests conducted during the years 1995 – 1997 while Unit 1 was combusting biomedical waste all demonstrated compliance with the applicable mercury emissions limits.⁵

Moreover, during the April 1998 stack tests, Unit 2 demonstrated compliance with the mercury emissions limits when combusting biohazardous waste at a rate equal to 90 to 100 percent of the permitted biohazardous waste feed rate for Unit 1. OMSL contends that those Unit 2 results are directly transferable to Unit 1, and are sufficient to demonstrate that, had Unit 1 been charged with biohazardous waste at a rate equal to 90 to 100 percent of the permitted biohazardous waste feed rate during the April 1998 tests, the Unit would have demonstrated compliance with applicable mercury emissions limits. There are several reasons why this is the case.

First, Units 1 and 2 each consist of a Martin GmbH Reverse-Reciprocating Stoker Grate and Heat Recovery/Steam Generator components manufactured by Zurn Industries. The Units are identical in design and construction and are capable of processing 264 tons per day of fuel at a Higher Heating Value of 5000 Btu/lb (equivalent to a heat input of 100 million Btu/hr). The design output is 64,418 lb/hr of steam at 830° F and 865 psig. The air pollution control systems serving each Unit also are identical, consisting of a scrubber and baghouse manufactured by Joy Environmental Equipment. The operating and maintenance procedures are the same for both Units 1 and 2.

Second, analysis of historical emissions data for Unit 1 versus Unit 2 demonstrates that there is no significant difference between the emissions from those Units. This is the case even though Unit 1 co-burns biohazardous waste with municipal solid waste, while Unit 2 burns solely municipal solid waste (with the exception of the April 1998 compliance test). Indeed, with respect to the actual test results for April 1998, statistical analysis of the inlet data for mercury for both Units demonstrates that it is unlikely that Unit 1 would have failed to meet the mercury emissions limit had that Unit

⁵ OMSL acknowledges that the January 1998 and January 1999 stack tests stand as exceptions to the general rule that Unit 1 is capable of meeting applicable mercury emissions limits while co-burning municipal solid waste and biohazardous waste. For the reasons stated elsewhere in this letter, however, OMSL firmly believes that the January 1998 and January 1999 tests were anomalous and not evidence of noncompliance.

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been charged at the permitted 2.15 ton/hr biohazardous waste feed rate, as opposed to the 1.12 tons/hr feed average biohazardous waste feed rate run during the stack test.⁶

Third, DEP's own regulations at 62-204.800(8)(b), F.A.C., incorporating by reference the federal "Subpart Cb" Emission Guidelines for Municipal Waste Combustors, including 40 C.F.R. 60.58b(g)(5)(iii), allow the results of compliance testing of one emissions unit at a facility to be used to demonstrate compliance for the same parameter for all units at the facility. Although that regulation applies specifically to compliance testing for dioxins and furans, the existence of the Rule demonstrates the merits of allowing facilities to make annual compliance demonstrations for like units through the testing of only one unit per year. If this alternative testing approach is feasible and appropriate for dioxins and furans – pollutants that, like mercury, are subject to control using carbon injection – there is no reason why it is also not feasible and appropriate for demonstrating compliance with mercury emissions limits. OMSL notes that the Department has the authority to allow such alternative compliance testing approaches pursuant to Rule 62-297.620, F.A.C.

Fourth, OMSL respectfully submits that the Department has been on notice of the throughput rates for biomedical waste burned during the April 1998 stack tests since July 1998, if not before (by virtue of the submission of the Environmental Test Report and the July 7, 1998 follow-up letter). The Warning Letter, however, represents the first formal notice provided to OMSL of the Department's position that Unit 1 should have been "de-rated" for biohazardous waste after the April 1998 stack tests. Although OMSL firmly believes that no harm to human health or the environment has resulted from its combustion of biohazardous waste in Unit 1 since April 1998, the Company nevertheless believes it regrettable that this issue of apparent concern to the DEP was not raised for mutual resolution well before the issuance of the Warning Letter.

In sum, available emissions data demonstrates that Unit 1 is capable of combusting biohazardous waste at the full 2.15 tons/hr rate without exceeding the applicable mercury emissions standard. OMSL demonstrated compliance with the mercury limits while combusting biohazardous waste on Unit 2 during the April 1998 stack tests, and such data are directly transferable to Unit 1. OMSL therefore contends that the facts demonstrate that Unit 1 should not be deemed to have been "de-rated" for biohazardous waste as a consequence of the April 1998 Unit 1 stack test conditions. Ample data exists to demonstrate that the underlying intent of Rule 62-297.310(2), F.A.C. has been satisfied. Equally importantly, there exists no evidence suggesting that

⁶ Indeed, the purpose of the testing for Unit 2 in April 1998 was to demonstrate that Unit 2 is identical in performance to Unit 1 with respect to the co-burning of municipal solid waste and biohazardous waste.

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human health or the environment were jeopardized as a result of operating Unit 1 at a biohazardous waste throughput rate of greater than 1.12 tons/hr in the wake of the April 1998 stack test.

For the foregoing reasons, the April 1998 stack testing performed on Unit 1 satisfied all applicable statutory, regulatory and permit requirements.

2. Unit 2

On page 2 of the Warning Letter, the Department suggests that the April 1998 mercury compliance test for Unit 2 was deficient because "the test was conducted with both municipal and biomedical waste, which should have been for the special tests only." This argument falls short of the mark for at least two reasons.

First, the Department's position represents a post hoc reinterpretation of the facts as they existed at the time of the April 1998 stack test. As previously discussed, that test was conducted in accordance with a DEP-approved protocol after protracted discussions between OMSL and DEP representatives about OMSL's proposal to combust biohazardous waste in Unit 2. In fact, the Warning Letter represents OMSL's first indication that the Department had any issues with respect to the conduct of the April 1998 testing of Unit 2. If the Department had any objections to the Source Test Plan with respect to Unit 2, those objections should have been raised prior to the conduct of the April 1998 tests. It is simply unfair for DEP to revisit that protocol over one year after the fact and now argue that OMSL's reliance on the Department's approval of the Source Test Plan somehow was misplaced.

Moreover, as discussed above, Units 1 and 2 are identical in construction and emission characteristics. As such, there is no basis for the Department's implicit suggestion that, had Unit 2 been tested while burning municipal solid waste alone, the Unit would have failed to demonstrate compliance with applicable mercury emissions limits. All evidence points to the contrary. Indeed, based on discussions held over time with Department representatives, most recently in April 1999 in Tallahassee, OMSL understands that the Department views the combustion of biohazardous waste as being a greater threat to the environment with respect to mercury emissions than the burning of municipal solid waste. Assuming, for the sake of argument, that the DEP's concerns about mercury in biohazardous waste are correct, it defies logic to assume that Unit 2 would have failed to demonstrate compliance with mercury limits in April 1998 had the unit been tested while burning *solely* municipal solid waste. The better view is that, if Unit 2 is capable of demonstrating compliance while co-burning biohazardous waste and municipal solid waste, then the Unit would be expected to demonstrate compliance when

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burning municipal solid waste alone. Indeed, OMSL has years of stack test data for Unit 2 proving that this is, in fact, the case.

For the foregoing reasons, the April 1998 stack testing performed on Unit 2 satisfied all applicable statutory, regulatory and permit requirements.

C. Regarding Tests Conducted January 26 Through January 29, 1999

1. Stack Test Results

During the time period from January 26 - 29, 1999, OMSL conducted stack tests on both Units 1 and 2 of the Facility to demonstrate compliance with, among other things, applicable mercury emission limits as required by Rule 62-296.416, F.A.C. and Permit AC35-264176. These tests were undertaken in accordance with Source Test Plan – OEG Report No. 2330, dated December 21, 1998, which previously had been submitted to the Department for review. As was the case in April 1998, the carbon injection rate to the air pollution control system during the stack testing was 11.2 lb/hr per Unit. Ms. Cindy Phillips of DEP's Tallahassee office was present during a portion of the stack tests.

A total of seven (7) sample runs were conducted, four (4) runs on Unit 1, and three (3) runs on Unit 2. The preliminary sampling results were received by OMSL from the testing laboratory in February. OMSL was surprised to find unprecedented inlet concentrations of mercury, as well as poor removal efficiencies. On February 17, 1999, OMSL's Jason Gorrie telephoned DEP's Gary Kuberski to provide a preliminary verbal report of the test results.

The final report for the January 1999 stack tests was delivered by hand by Mr. Gorrie to DEP's Central Office on March 16, 1999, under a cover letter dated March 12, 1999 (see Environmental Test Report – OEG Report No. 2373, dated March 8, 1999). At this time, Mr. Gorrie discussed the results of testing with DEP personnel, including Gary Kuberski, Leonard Kozlov, John Turner, Saadia Qureshi, and Caroline Shine. As discussed at that meeting, and as stated in the cover letter to the Environmental Test Report, “[t]he Unit 1 mercury results indicated concentrations that were well outside the known database of any WTE facility. The results for Unit 2 did not demonstrate compliance with the emission limit.” See Letter dated March 12, 1999 from G.J. Aldina, Sr. Vice President, Environmental Testing/CEM, Ogden Energy Group, Inc., to Gary Kuberski, DEP (attached as Exhibit 8).

A revised copy of the final stack test results was submitted to the Department on March 29, 1999 (see Environmental Test Report – OEG Report No. 2373R, dated March 26, 1999). (The Report was revised to convert the mercury emission concentrations from

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Central District
Florida Department of Environmental Protection
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the originally reported presentation at 12% CO₂ to concentrations expressed at 7% O₂). The revised Report, at page 1 of the Executive Summary (Volume 1), characterized the conduct and results of the mercury sampling, as follows:

The mercury emission data for both units are not consistent with the control efficiency expected with activated carbon injection systems. The carbon injection system at the facility operated in accordance with permit requirements at all times without malfunction. The laboratory analysis for mercury was conducted twice.

A copy of Volume 1 of the Environmental Test Report is attached as Exhibit 9.

After receiving the results from the January 1999 stack tests, OMSL undertook additional stack testing in February 1999 to confirm that the January results indeed were an anomaly. As indicated by the data provided to the Department both in the March 12, 1999 Environmental Test Report (OEG Report No. 2374) and at an April 29, 1999 meeting between DEP and OMSL/OEG representatives, the mercury results at the time of the February stack test were well within the applicable emission limiting standard for mercury.

OMSL's post-January 1999 efforts were not limited to additional stack testing. The Company undertook certain efforts with respect to the carbon injection system, and also began internal investigations to determine the possible source(s) of wastestream mercury contamination. With respect to the carbon injection system, OMSL calibrated the system and ultimately increased the carbon injection rate to 23 lbs/hr (as of the April 1999 stack tests). OMSL also sampled the carbon to determine whether any "contamination" issues exist with respect to that material (there were none), and conducted mercury speciation tests. In sum, contrary to the Department's suggestion at page 5 of the Warning Letter, there was no evidence to support the view that the January 1999 stack test results were attributable to any technological or operational problems at the Facility.

Based on the operating experience of OMSL and its sister companies in Florida and elsewhere, the Company strongly suspected that the January 1999 results had to be the result of a problem with the incoming wastestream. Accordingly, OMSL immediately set about to identify any unusual sources of mercury in the area that might be reaching the Facility. As a result of this investigation, OMSL strongly suspected that a likely source of mercury-contaminated materials in the wastestream was Florida Medical Industries ("FMI"), located in Fruitland Park, Lake County.⁷

⁷ OMSL representatives raised the possibility that FMI was a source of mercury materials entering the Facility during the referenced March 26, 1999. At that time, however, OMSL had no conclusive evidence that FMI indeed was disposing mercury containing

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After identifying FMI as a potential source of mercury contaminated materials in the municipal wastestream, OMSL implemented a stepped-up inspection program for waste coming into the Facility from one particular municipal waste pick-up route. While the company's internal waste inspection procedures contemplate random inspections of typically six (6) loads per day, OMSL began targeting all incoming trucks from the questionable route for inspection in early to mid-March. In addition, the Facility purchased a "Jerome" meter to aid in the detection of elemental mercury vapors from suspect loads of waste and began using that instrument in early to mid-April when the Facility came out of a scheduled outage.

As a result of the visual inspection and vapor monitoring initiated in March, OMSL personnel discovered the mercury-containing materials in a truckload of waste delivered on April 22, 1999 -- literally moments before mercury stack testing was to begin. Visual observation of the mercury-contaminated materials -- including, among other things, broken mercury thermometers and packaging containing free-flowing mercury -- revealed that certain items were labelled as FMI products. Due to concern that some of the contaminated materials could have gotten into the pit and that mercury vapors from the waste materials was being drawn in to the air intakes to the Units, OMSL decided to postpone a portion of the compliance testing. As the Department is aware, OMSL was able to complete the scheduled compliance test for Unit 2 on that date; however, compliance testing at Unit 1 did not take place the following day. Compliance testing for Unit 1 instead was undertaken on June 3, 1999. As reported in the Environmental Test Reports for the April and June 1999 stack tests, both Unit 1 and Unit 2 have been shown to be in compliance with applicable mercury emission limits. See Environmental Test Report (OEG Report No. 2398) (dated June 8, 1999) (April 1999 test), and Environmental Test Report (OEG Report No. 2404) (dated June 22, 1999) (June 1999 test).

In light of the foregoing chain of events, OMSL contends that enforcement action with respect to the January 1999 stack test is not warranted. First, a comparison of the January 1999 stack test results with both past and subsequent mercury test results supports OMSL's contention that the high inlet loadings of mercury and poor mercury

waste in the municipal wastestream, and the Department offered no opinion on this issue. As further discussed below, OMSL has since obtained documents from DEP's files demonstrating that FMI indeed was disposing of mercury contaminated materials in the municipal wastestream during the relevant time period, and that DEP had knowledge of this disposal practice. OMSL also has learned that materials from FMI likely arrived at the OMSL Facility during the January 1999 stack test.

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removal efficiencies were attributable to an unusual, unanticipated, and illegal⁸ source of mercury in the waste stream. There is absolutely no evidence to suggest that the problem was caused by any technological or operational failures at the facility. On the contrary, records of waste deliveries to the Facility demonstrate that, on January 27, 1999, a truckload of waste from the municipal route that includes FMI was delivered to OMSL, the same day upon which mercury stack testing was occurring.⁹ In view of this evidence, OMSL contends that the anomalous and unprecedented mercury stack testing results for January 1999 resulted directly from contamination of the incoming wastestream by mercury materials that were improperly disposed of by the generator, apparently in reliance upon a DEP-approved site cleanup protocol.

Second, any enforcement action against the Facility would penalize the operator for an event that is essentially out of its control. As indicated above, OMSL has implemented a comprehensive waste screening procedure at Facility that exceeds the industry standard or any regulatory requirements. In addition, even more extensive screening procedures were self-imposed by OMSL once it became aware of a specific, suspected source of mercury in the wastestream. It should be obvious that it is not possible, for operational, economic, and employee health and safety reasons, to check every load of waste coming into the facility on an ongoing basis. OMSL strongly believes that its screening process is more than adequate under normal circumstances and demonstrates the Facility's good faith efforts to assure compliance. Indeed, these screening procedures in all likelihood prevented a stack test failure from occurring in April 1999. Equally importantly, OMSL's discovery and segregation of the mercury waste materials from the waste feed to the Units also prevented the cross-media transfer of mercury into the atmosphere.

Third, and perhaps most significantly, OMSL remains concerned that it was never notified by the Department of the existence of FMI as a potential source of mercury contaminated waste, particularly in light of that company's documented record of past non-compliance with hazardous waste laws. This omission is even more difficult to understand in light of the fact that OMSL brought that possibility to the attention of the Department shortly after the January testing. Documentation since obtained by OMSL during a file review at the Central District indicates that Department officials had knowledge that FMI was involved in a hazardous waste site cleanup that featured the "final disposal" of mercury-contaminated waste materials via "remov[al] from the site by

⁸ The disposal of "mercury-containing devices," such as mercury thermometers, via incineration is prohibited by Section 403.7186, F.S.

⁹ A spreadsheet setting forth all deliveries to the Facility from November 1998 through April 22, 1999 from the specific municipal route that serves FMI is attached as Exhibit 10.

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Town and County (waste hauler) and transport[ation] to the Lake County incinerator.”¹⁰ OMSL contends that it is inequitable for the Department to attempt to penalize the Facility for the results of the January 1999 stack test under these circumstances. Whether technically “hazardous” or not, the fact remains that mercury-contaminated materials from the FMI site should never have been allowed by the Department to be placed in the municipal wastestream for “final disposal” at the Facility. Such disposal is contrary to Section 403.7186, F.S., which prohibits the disposal of mercury-containing articles at waste-to-energy facilities – regardless of whether or not those articles are “hazardous wastes” – to prevent the release of mercury to the environment.

Finally, all of the testing at the Facility points to the fact that the exceedance of the mercury emission standard which the Facility experienced in January 1999 was a one-time event of short duration. The subsequent February 1999 stack tests, although not conducted as “compliance tests,” demonstrate that the Facility was in compliance by those dates, if not sooner. The compliant status of the Facility with respect to mercury is further supported by the results of the April 1999 and May 1999 stack tests for Unit 1 and Unit 2, respectively. For all these reasons, OMSL contends that enforcement by the Department with respect to the January 1999 stack test is wholly unwarranted.

2. January 1999 Environmental Test Report

The Warning Letter at page 2 asserts that OMSL failed to provide certain information in the stack test report submitted to the Department for the January 1999 tests. OMSL disagrees with this assertion. Volume III of the Environmental Test Report for the January 1999 tests includes all of the information required by 62-297.310(8) F.A.C., and specifically provides the information necessary to determine: (1) the medical waste rate in tons/hr; (2) the municipal solid waste rate in pounds-steam/hour; and (3) the emission rates for Run 1 on Unit 1.¹¹ Nevertheless, as requested by DEP, the medical

¹⁰ See Interim Remedial Action Plan, Florida Medical Industries, Inc., Leesburg, Lake County, Florida (October 1995) at page 3-4 (excerpt attached as Exhibit 11). FMI was required to undertake this cleanup by a DEP-issued Consent Order (File No. 94-1594) resulting from a DEP investigation of illegal mercury hazardous waste disposal at the site.

¹¹ OMSL understands that these three items of information, listed on page 2 of the Warning Letter, are the same items referenced on page 6 of the Warning Letter as “the process rates of the January 1999 tests.” Additional information requested by DEP at page 6 of the Warning Letter, referred to as “copies of all operational log documentation and waste burned identification and quantity, including the day prior to and for the period of the January 1998 and [January] 1999 test, are provided as Exhibits 12 and 13.

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waste feed rate in tons/hr for each run of the January 1999 stack test, as well as the steam flow in pounds-steam/hour for each test run, is provided in the table below:

Lake Process Summary
January 27, 1999

	RUN	Average Steam flow klbs/hr	Total Medical Waste	
			lbs	tons/hr
0840-1111	1	62.5	7045.2	1.40
1140-1350	2	61.8	6976.2	1.61
1420-1648	3	64.5	10853.4	2.31
1713-1920	4	62.9	7916.8	1.87

OMSL notes that, as discussed in the Environmental Test Report for the January 1999 stack tests, the final, calculated results of Run 1 were not included in the final average biohazardous waste rate.

With respect to the Unit 1, run 1 mercury emission rates referenced at page 2 of the Warning Letter, the Environmental Test Report included all of the stack test data and laboratory analysis that is necessary to accurately calculate those rates. The supporting information can be found in Appendix A, pages 005 and 010, Appendix B.3, page 78A-B, Appendix B.4, page 88A-B, and Appendix C.2, page 227A. These pages are provided as Exhibit 14 to this letter, along with a completed summary provided by Testar, Inc. Information provided in the Environmental Test Report for the January 1999 stack tests and the mercury emission rates were discussed with Mr. Gary Kuberski of DEP during the March 25, 1999 pre-test meeting at the Facility in advance of the April 1999 stack testing.

II. ISSUES REGARDING RECORD REVIEW

A. Medical Waste Delivery Report: January 26, 1999

The Warning Letter, at page 3, makes reference to a January 26, 1999 delivery of biohazardous waste to the Facility, which delivery included two boxes labeled "chemotherapy waste/hazardous drug waste." This delivery was among the subjects addressed in a May 17, 1999 Request for Information directed to OMSL by Robert T. Snyder, P.E., Program Manager, Hazardous Waste Section, Central District Office, DEP.

OMSL provided its response to the Request for Information by letter dated June 2, 1999 from Cecil D. Boatright, Facility Manager, OMSL, to DEP's Robert T. Snyder. OMSL has since learned that DEP representatives have visited the generator of the

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subject biohazardous waste boxes, and that the generator provided the Department with additional documentary and other information demonstrating that the chemotherapeutic drug wastes in question were not subject to regulation as hazardous wastes. OMSL is not aware of any further DEP action with respect to this issue, and respectfully submits that no further action is warranted, insofar as no violation of law has occurred.

B. Records of Carbon Injection Rate

The Warning Letter at page 3 alleges certain "discrepancies" in OMSL's recordkeeping as it pertains to carbon use at the Facility. As further discussed below, any such "discrepancies" noted by the Department are of no legal or practical significance. OMSL is in full compliance with all carbon injection rate recordkeeping requirements.

The carbon injection rate for each Unit at the Facility is recorded by the continuous emission monitoring ("CEM") system. The CEM records the carbon rate in engineering units (lb/hr). Each Unit's carbon injection system feeds carbon to the air pollution control equipment using an auger feeder and air eductor. The rotation speed (RPM) of the auger is proportional to the mass feed rate (lb/hr). The required mass feed rate for each Unit is 11.2 lb/hr. The auger RPM which represents 11.2 lb/hr feed is established during the annual emission test. (OMSL notes that the carbon feed rate calibration was observed by DEP's Caroline Shine and Garry Kuberski during the Facility's June 3, 1999 stack test.) The individual carbon injection control systems send an isolated, electrical output proportional to the lb/hr injection rate of the system to the CEM for recording. The CEM system records the signal as the engineering unit of lb/hr. The CEM data acquisition system stores the carbon injection rate data for each Unit to the CEM network computer. Those data are archived to reliable storage media and kept at the Facility. The CEM data are reported in the "Daily Process Summary Continuous One Hour Sheets" referenced at page 3 of the Warning Letter. The foregoing procedures for establishing the carbon injection rate and continuously recording that rate are consistent with 40 C.F.R. 60.58b(m)(1)-(2) requirements, as incorporated by reference at 62-296.416(5).

The total carbon injection rate for the Facility is determined from the carbon purchases. The carbon injection system includes a carbon storage silo above the auger feeders. This main silo feeds the individual carbon bins directly above each auger feeder. The main silo has carbon level sensors that indicate the approximate height of the carbon in the silo. The silo is filled with new carbon purchases as needed to assure adequate carbon for operation of the system. The carbon purchases are based on experience with carbon use by the system (feed rate of carbon; silo level; estimated density of carbon per cubic volume-estimated pounds of carbon in the silo). The amount of carbon purchased varies according to the silo indicators and the availability of vendor delivery. There is

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typically at least 30 days of carbon at site for both Units at all times. The foregoing procedures are used to determine the quarterly carbon use rate, consistent with 40 C.F.R. 60.58(m)(3) requirements.

Turning to the issue of alleged “discrepancies” between carbon usage rates as recorded by the CEM system (the so-called “Daily Process Summary Continuous One Hour Sheets”) and as logged in the Daily Production Reports, it is important to understand that the Daily Production Reports (1) are not intended to demonstrate compliance with the required carbon injection rate, and (2) are not used by OMSL to comply with carbon injection requirements. Instead, the carbon usage data set forth in the Daily Production Reports are used by OMSL solely as an internal accounting method for scheduling deliveries of carbon to the Facility.

The carbon use calculation included in each Daily Production Report is calculated by multiplying the total hours of unit operation for that day “times” the carbon injection rate in pounds per hour. This calculation is done using a spreadsheet program, with the carbon injection rate in lbs/hr established as a fixed value in the spreadsheet program equal to the rate established during the previous compliance test. The “variable” in this carbon use equation is the total hours of unit operation, which is manually entered by Facility personnel.

During a June 3, 1999 Facility inspection, DEP’s Caroline Shine noted that the carbon usage rates as recorded by the CEM system during the period from April 21 through June 3 were different than the carbon usage rates recorded in the Daily Production Reports for the same time period. As was explained to DEP during that inspection, the differential between the two record types was traceable to an error in the spreadsheet program used to generate the Daily Production Report; namely, the pre-programmed carbon injection rate in the spreadsheet had not been changed from the “old” 11.2 lb/hr injection rate to the “new” 23 lb/hr injection rate established in the April 1999 compliance test (on April 21). The spreadsheet program has since been corrected to include the correct 23 lb/hr carbon injection rate. As requested by the Department at page 3 of the Warning Letter, copies of “the two Carbon Injection Rate Reports for the entire period of January 1999 through June 3, corrected and uncorrected,” are attached, as follows: Exhibit 15 (Daily Production Sheets April 21 – June 3, 1999 (“corrected”)); Exhibit 16 (Daily Production Sheets January 1999 – June 3, 1999 (“uncorrected”)); and Exhibit 17 (CEM-recorded carbon injection data January – June 3, 1999).¹²

¹² OMSL notes that, because the carbon injection rate for the time period January 1999 through April 20, 1999 was correctly entered in the spreadsheet program, the Daily Production Reports for that timeframe are not in need of “correction.” Similarly, the CEM-recorded carbon injection data for the entire period from January through June 3, 1999 is correct.

Vivian F. Garfein
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In summary, the error noted by DEP in the carbon usage rate calculation in the Daily Production Report during the time period from April 21 to June 3, 1999 was of no practical or legal significance. Notwithstanding that error, OMSL had sufficient quantities of carbon on-site at all times to ensure compliance with applicable lb/hr carbon injection rate. Moreover, the CEM system was properly calibrated to ensure that carbon injection rates were accurately recorded and the quarterly carbon usage calculation was properly conducted, all in accordance with 40 C.F.R. 60.58b(m). For all of these reasons, OMSL contends that the Facility has been and continues to be in compliance with carbon usage and recordkeeping requirements, such that no violation of law exists.

* * *

For the foregoing reasons, OMSL contends that the Facility has been and remains in compliance with applicable statutes, regulations and permit requirements, and thus that the issues of alleged noncompliance raised by the Warning Letter are without merit.

OMSL looks forward to the opportunity to discuss the Warning Letter and OMSL's response thereto directly with the Department. OMSL will be in contact with the Department shortly to propose meeting dates and times after first consulting with Lake County officials regarding scheduling. In the meantime, if you have any questions about this response of OMSL, please feel free to contact Mary F. Smallwood, Esq. at (850) 681-9027.

Sincerely yours,

Gary K. Crane / ncc

Gary K. Crane, Ph.D.
Executive Vice President, Environmental

Enclosures

Vivian F. Garfein
Director of District Management
Central District
Florida Department of Environmental Protection
July 15, 1999
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cc: Susan Whittle, County Manager, Lake County
Sanford Minkoff, Esq., County Attorney, Lake County
Caroline Shine, DEP – Orlando
Leonard Kozlov, DEP – Orlando
Garry Kuberski, DEP – Orlando
Robert Snyder, DEP – Orlando
Clair Fancy, DEP – Tallahassee
Mike Halpin, DEP – Tallahassee
Scott Sheplak, DEP – Tallahassee
Al Linero, DEP – Tallahassee
Mary F. Smallwood, Esq.

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July 2, 1999

RECEIVED

JUL 16 1999

BUREAU OF AIR REGULATION

Vivian Garfein, Director
Central District
Department of Environmental Protection
3319 Maguire Blvd, Suite 232
Orlando, Florida 32803-3767

Re: Response to Warning Letter OWL-AP-99-413

Dear Vivian:

We are in receipt of Warning Letter OWL-AP-99-413 issued to Ogden Martin Systems of Lake, Inc. ("OMSL") and dated June 15, 1999. The Warning Letter, which was received on June 18, 1999, requests that a written response be submitted to the Department and that OMSL contact the Department within fifteen days of receipt of the letter to arrange a meeting. As we discussed by telephone, OMSL is presently preparing a written response to the Warning Letter. That response will be submitted as soon as possible but no later than July 16, 1999. Because there were a number of complex issues raised in the Warning Letter, OMSL needs that time to assure that its written response is as complete as possible.

In addition, this letter is intended to serve as OMSL's request for a meeting with appropriate Department personnel to discuss the allegations in the Warning Letter. It would seem to be most appropriate to schedule that meeting after the Department has had a chance to review our written response. We will contact Caroline Shine directly within the next week with dates that are available to OMSL for such a meeting.

Thank you for your consideration in this matter.

Sincerely,

RUDEN, McCLOSKEY, SMITH,
SCHUSTER & RUSSELL, P.A.

Mary F. Smallwood

Mary F. Smallwood

MFS/mb
cc: Caroline Shine
Nancy Tammi
Gary Crane

40 Lane Road
Fairfield, NJ 07007
973 882 9000
Fax 973 882 4156

March 11, 1998

Mr. Anatoliy Sobolevskiy
Air Resources Management
Florida Department of Environmental Protection
Central Division
3319 Maguire Boulevard, Suite 232
Orlando, Florida 32803-3767

RECEIVED
MAR 11 1998
O.M.S. OF LAKE

Subject: OMS of Lake, Inc.
Lake County Resource Recovery Facility
Compliance Test Report

Dear Mr. Sobolevskiy:

Enclosed is the environmental test report for the annual emissions testing and relative accuracy test audit (RATA) performed at the Lake County Resource Recovery Facility on January 27-29, 1998. This testing was conducted in accordance with the State of Florida Department of Environmental Protection, Permit/Certification No. A035-193817, Rule 62-296.416(3)(a)1 and 40 CFR 60, Appendices B & F.

The mercury results for Units 1 and 2 were not consistent with results expected for systems with carbon injection. These results, as discussed with you by Jason Gorrie on February 29, 1998, do not seem possible with carbon injection systems for mercury control. We can discuss these results with you after your review of the test report.

Please contact me at (973) 882-7173 if you have any questions.

Sincerely,

 for

Michelle L. Genberg
Manager - Reports

RECEIVED
MAR 25 1998
O.M.S. OF LAKE

MLG:rj
Enclosure

- cc: D. Crowe - Lake Co. (w/Encl.)
- G. J. Aldina
- G. Crane
- C. Boatwright (w/Encl.)
- J. Gorrie (w/Encl.)
- L. Simpson (w/RATA)

40 Lane Road
Fairfield, NJ 07007
973 882 9000
Fax 973 882 4156

ENVIRONMENTAL TEST REPORT

VOLUME 1

EXECUTIVE SUMMARY - OEG Report No. 2252

March 6, 1998

PREPARED FOR: Ogden Martin Systems of Lake, Inc.
3830 Rogers Industrial Park
P. O. Box 189
Okahumpka, Florida 34762

PURPOSE: To Demonstrate Compliance with Florida Department of
Environmental Protection, Permit No. AO35-193817 and
Rule 62-296.

TEST DATES: January 27-29, 1998

ASSOCIATED REPORTS: OEG Report No. 2193

PREPARED BY: Ogden Energy Group, Inc.
Department 38 - CEM/Emission Testing



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VOLUME 2: Air Kinetics, Inc. Report on Compliance Testing
(Bound Separately)

VOLUME 3: Confidential Process Data
(Bound Separately)

1.0 INTRODUCTION

Ogden Martin System of Lake, Inc, (OMSL) performed compliance emission tests at the Lake County Resource Recovery Facility from January 27-29, 1998. The purpose of this test program was to demonstrate compliance with the Florida Department of Environmental Protection (FLDEP), Permit No. AO35-193817, Specific Condition 8 and Rule 62-296. The testing was performed by Air Kinetics, Inc. (AKI) in accordance with all procedures in the FLDEP approved test protocol.

The OMSL municipal solid waste combustion facility is located in Okahumpka, FL. The facility is rated at 528 tons of municipal solid waste per day. Units 1 and 2 were tested for mercury emissions at the economizer outlet and stack. Acid gas emissions were tested at the inlet and outlet of the air pollution control equipment. All testing was conducted simultaneously in accordance with procedures required by Florida Department of Environmental Protection (FLDEP) regional office.

A summary of emission test results for the facility is presented in Section 2.0, Tables 2.1 and 2.2. The AKI report (Volume 2) includes all testing data gathered at the site and all laboratory analytical data.

The test program, as indicated in the Source Test Plan (OEG Report No. 2193), is presented in Section 3.0, Table 3.2. Test observers and participants are presented in Table 3.1. The Schedule of Activities is presented in Table 3.3.

The mercury emission data for both units are not consistent with the control efficiency expected with activated carbon injection systems. The carbon injection system at the facility operated in accordance with permit requirements at all times without malfunction. The laboratory analysis for mercury was conducted twice. The results of the second analysis appear in the following tables. The results from the original analysis can be found in the appendices of Air Kinetics's report, Volume 2.

2.0 SUMMARY OF RESULTS

TABLE 2.1
SUMMARY OF SOURCE TEST RESULTS - UNIT 1

Pollutant	----- Replicate ⁽¹⁾ -----			Average	Permitted Compliance Emission Limits
	1	2	3		
<u>SDA INLET</u>					
<u>Conc., ppmdv @ 12% CO₂</u>					
Sulfur Dioxide (SO ₂)	35.8	27.0	21.3	28.0	-----
<u>Emission Rate, lb/hr</u>					
Mercury (Hg)	0.0380	0.0180	0.0387	0.0316	-----
Hydrogen Chloride (HCl)	175	197	118	163	-----
<u>STACK ⁽²⁾</u>					
<u>Conc., ppmdv @ 7% O₂</u>					
Hydrogen Chloride (HCl)	56.6	72.6	25.7	51.6	50
Carbon Monoxide (CO)	23.5	21.6	23.0	22.7	100
<u>Conc., ppmdv @ 12% CO₂</u>					
Sulfur Dioxide (SO ₂)	25.0	23.2	5.6	17.9	60
Nitrogen Oxides (NO _x)	245	266	255	256	385
<u>Conc., gr/dscf @ 7% O₂</u>					
Particulate Matter (PM)	2.08E-03	4.74E-03	3.56E-03	3.46E-03	0.02
<u>Conc., gr/dscf @ 12% CO₂</u>					
Particulate Matter (PM)	2.22E-03	4.62E-03	3.50E-03	3.45E-03	0.015
Mercury (Hg)	1.31E-04	7.22E-05	5.20E-05	8.51E-05	3.4E-04
<u>Conc., ug/dscm @ 7% O₂</u>					
Mercury (Hg)	309	174	123	202	70
<u>Emission Rate, lb/hr</u>					
Mercury (Hg)	0.0325	0.0176	0.0125	0.0209	-----
Hydrogen Chloride (HCl)	9.31	11.8	4.20	8.44	-----
<u>Removal Efficiency, %</u>					
Hydrogen Chloride (HCl) ⁽³⁾	94.7	94.0	96.4	95.0	≥90
Mercury (Hg) ⁽³⁾	14.3	2.22	67.7	28.1	≥80
Sulfur Dioxide (SO ₂) ⁽⁴⁾	30.2	14.1	73.7	39.3	≥70
<u>Opacity, %</u>					
Visible Emissions (VE)	0	0	0	0	15

⁽¹⁾ Data presented as repetition number. Actual sample run number may differ.

⁽²⁾ All testing for HCl, SO₂, NO_x, CO, opacity, and particulate done simultaneously.

⁽³⁾ Based on lb/hr.

⁽⁴⁾ Based on ppmdv @ 12% CO₂.

TABLE 2.2

SUMMARY OF SOURCE TEST RESULTS - UNIT 2

Pollutant	----- Replicate -----			Average	Permitted Compliance Emission Limits
	1	2	3		
<u>SDA INLET</u>					
<u>Conc., ppmvd @ 12% CO₂</u>					
Sulfur Dioxide (SO ₂)	39.3	41.3	47.8	42.8	-----
<u>Emission Rate, lb/hr</u>					
Mercury (Hg)	0.0186	0.0216	0.0128	0.0177	-----
Hydrogen Chloride (HCl)	97.8	83.4	90.0	90.4	-----
<u>STACK ⁽¹⁾</u>					
<u>Conc., ppmvd @ 7% O₂</u>					
Hydrogen Chloride (HCl)	25.8	18.9	36.7	27.1	50
Carbon Monoxide (CO)	20.7	16.1	20.7	19.2	100
<u>Conc., ppmvd @ 12% CO₂</u>					
Sulfur Dioxide (SO ₂)	15.7	4.80	29.1	16.5	60
Nitrogen Oxides (NO _x)	343	350	274	322	385
<u>Conc., gr/dscf @ 7% O₂</u>					
Particulate Matter (PM)	1.32E-02	3.77E-03	5.46E-03	7.48E-03	0.02
<u>Conc., gr/dscf @ 12% CO₂</u>					
Particulate Matter (PM)	1.34E-02	3.64E-03	5.28E-03	7.44E-03	0.015
Mercury (Hg)	8.43E-05	2.48E-05	2.01E-05	4.31E-04	3.4E-04
<u>Conc., ug/dscm @ 7% O₂</u>					
Mercury (Hg)	202	59.5	48.2	103	70
<u>Emission Rate, lb/hr</u>					
Mercury (Hg)	0.0211	0.00611	0.00486	0.0107	-----
Hydrogen Chloride (HCl)	4.08	3.01	5.72	4.27	-----
<u>Removal Efficiency, %</u>					
Sulfur Dioxide (SO ₂) ⁽²⁾	60.1	88.4	39.1	62.5	≥70
Hydrogen Chloride (HCl) ⁽³⁾	95.8	96.4	93.6	95.3	≥90
Mercury (Hg) ⁽³⁾	-13.4	71.7	62.0	40.1	≥80
<u>Opacity, %</u>					
Visible Emissions (VE)	0	0	0	0	15

⁽¹⁾ All testing for HCl, SO₂, NO_x, CO, opacity, and particulate done simultaneously.

⁽²⁾ Based on ppmvd @ 12% CO₂.

⁽³⁾ Based on lb/hr.

3.0 TEST PROGRAM

TABLE 3.1
TEST PARTICIPANTS

Ogden Energy Group, Inc.

G. J. Aldina

Air Kinetics, Inc.

Shawn Graham
Gary Mata
Son Bui
Wayne Johnson
Tony Wong
Alfred Guzman

Florida Department of Environmental Protection

Gary Kuberski

Malcolm Pirnie

John Pacifici

Beatty Environmental Services

Daniel Beatty

TABLE 3.2
TEST PROGRAM

Parameter	Method
Particulate Matter (PM)	U.S. EPA Method 5
Sulfur Dioxide (SO ₂) ⁽¹⁾	U.S. EPA Method 6C
Nitrogen Oxides (NO _x)	U.S. EPA Method 7E
Carbon Monoxide (CO)	U.S. EPA Method 10
Visible Emissions (VE)	U.S. EPA Method 9
Hydrogen Chloride (HCl) ⁽¹⁾	U.S. EPA Method 26
Mercury (Hg) ⁽¹⁾	U.S. EPA Method 29

⁽¹⁾ SO₂, HCl and Hg sampled at the inlet and outlet of the air pollution control equipment.

TABLE 3.3
SCHEDULE OF ACTIVITIES

Date/ Time	Unit	Location	Sampling Method	Replicate (Run)	Parameter
<u>1/27/98</u>					
0951-1051	1	Outlet	EPA 9	1	VE
0951-1207	1	Outlet	EPA 5	1	PM
0951-1207	1	Inlet	EPA 26	1	HCl
0953-1208	1	Outlet	EPA 26	1	HCl
0956-1055	1	Inlet	EPA 3A, 6C	1	O ₂ , CO ₂ , SO ₂
0956-1055	1	Outlet	EPA 3A, 6C, 7E, 10	1	O ₂ , CO ₂ , SO ₂ , NO _x , CO
1355-1618	1	Outlet	EPA 5	2	PM
1355-1631	1	Inlet	EPA 26	2	HCl
1358-1628	1	Outlet	EPA 26	2	HCl
1405-1505	1	Outlet	EPA 9	2	VE
1406-1505	1	Inlet	EPA 3A, 6C	2	O ₂ , CO ₂ , SO ₂
1406-1505	1	Outlet	EPA 3A, 6C, 7E, 10	2	O ₂ , CO ₂ , SO ₂ , NO _x , CO
1742-1825	1	Outlet	EPA 9	3	VE
1742-1945	1	Inlet	EPA 26	3	HCl
1743-1952	1	Outlet	EPA 5	3	PM
1744-1956	1	Outlet	EPA 26	3	HCl
1758-1857	1	Inlet	EPA 3A, 6C	3	O ₂ , CO ₂ , SO ₂
1758-1857	1	Outlet	EPA 3A, 6C, 7E, 10	3	O ₂ , CO ₂ , SO ₂ , NO _x , CO
<u>1/28/98</u>					
0825-1034	2	Inlet	EPA 26	1	HCl
0825-1038	2	Outlet	EPA 5	1	PM
0827-1032	2	Outlet	EPA 26	1	HCl
0830-0930	2	Outlet	EPA 9	1	VE
0923-1022	2	Inlet	EPA 3A, 6C	1	O ₂ , CO ₂ , SO ₂
0923-1022	2	Outlet	EPA 3A, 6C, 7E, 10	1	O ₂ , CO ₂ , SO ₂ , NO _x , CO
1130-1343	2	Outlet	EPA 5	2	PM
1130-1355	2	Inlet	EPA 26	2	HCl
1131-1230	2	Inlet	EPA 3A, 6C	2	O ₂ , CO ₂ , SO ₂
1131-1230	2	Outlet	EPA 3A, 6C, 7E, 10	2	O ₂ , CO ₂ , SO ₂ , NO _x , CO
1132-1337	2	Outlet	EPA 26	2	HCl
1135-1235	1	Outlet	EPA 9	2	VE
1135-1235	1	Outlet	EPA 9	3R	VE
1505-1719	2	Outlet	EPA 5	3	PM
1505-1714	2	Inlet	EPA 26	3	HCl
1506-1720	2	Outlet	EPA 26	3	HCl
1510-1610	2	Outlet	EPA 9	3	VE
1556-1655	2	Inlet	EPA 3A, 6C	3	O ₂ , CO ₂ , SO ₂ , NO _x , CO
1556-1655	2	Outlet	EPA 3A, 6C, 7E, 10	3	O ₂ , CO ₂ , SO ₂ , NO _x , CO
<u>1/29/98</u>					
0900-1150	1	Outlet	EPA 29	1	Hg
0900-1150	2	Outlet	EPA 29	1	Hg
0900-1151	1	Inlet	EPA 29	1	Hg
0902-1151	2	Inlet	EPA 29	1	Hg
1247-1516	1	Inlet	EPA 29	2	Hg
1247-1524	2	Outlet	EPA 29	2	Hg
1248-1519	1	Outlet	EPA 29	2	Hg
1249-1524	2	Inlet	EPA 29	2	Hg
1618-1850	1	Outlet	EPA 29	3	Hg
1618-1850	2	Outlet	EPA 29	3	Hg
1619-1850	1	Inlet	EPA 29	3	Hg
1621-1852	2	Inlet	EPA 29	3	Hg

4.0 OPERATIONAL DATA DURING EMISSION TESTING

4.0 OPERATIONAL DATA DURING EMISSION TESTING

Operational data were collected from process recorders. This confidential data is shown in Volume 3.

—

5.0 METHODOLOGY

TABLE 5.1
REFERENCES

Parameter	Test Method	Reference
PM	U.S. EPA Method 5	40 CFR 60, App. A
SO ₂	U.S. EPA Method 6C	40 CFR 60, App. A
NO _x	U.S. EPA Method 7E	40 CFR 60, App. A
CO	U.S. EPA Method 10	40 CFR 60, App. A
VE	U.S. EPA Method 9	40 CFR 60, App. A
HCl	U.S. EPA Method 26	40 CFR 60, App. A
Hg	U.S. EPA Method 29	40 CFR 60, App. A

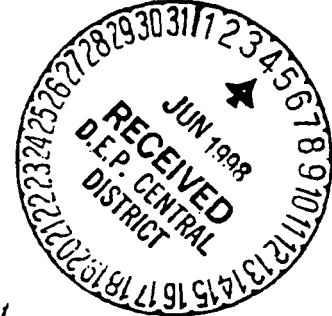
4

OGDEN

June 2, 1998

Ogden Martin Systems of Lake, Inc.
3830 Rogers Industrial Park Rd.
Okahumpka, FL 34762
352 365 1611
Fax 352 365 6359

Mr. Leonard Kozlov, P.E.
Florida Department of Environmental Protection
Air Management Program
3319 Maguire Blvd.
Suite 232
Orlando, Florida



*SUBJ: Compliance Testing Results - Mercury Retest
Lake County Resource Recovery Facility*

Dear Mr. Kozlov:

Attached, please find the results of mercury emissions testing conducted at Ogden Martin Systems of Lake, Inc. on April 21, 22, and 23, 1998. As you are aware, the results from mercury stack testing in January indicated likely sample contamination. As a result, and, following discussions with Dr. Anatoliy Sobolevskiy of your staff, a re-test was undertaken in order to demonstrate compliance with the mercury emission limiting standard found at 62-296.413, F.A.C. You will also be receiving, under separate cover, results of stack testing conducted on Unit #2 while firing medical waste.

Thank you for your assistance in this matter. If additional information is needed, please contact me at (352) 365-1611.

Sincerely,

A handwritten signature in black ink, appearing to read "Jason M. Gorrie".

Jason M. Gorrie
Senior Environmental Engineer
Ogden Martin Systems of Lake, Inc.

ENGINEERING TEST REPORT

UNIT NOS. 1 AND 2

Source Location:

**Ogden Martin Systems of Lake, Inc.
3830 Rogers Industrial Park
Okahumpka, Florida 34762**

Test Date: March 3 and 4, 1998

Issue Date: April 21, 1998

Revision: 0

Prepared for:

**Ogden Energy Group, Inc.
40 Lane Road
Fairfield, New Jersey 07007**

Prepared by:

**AirKinetics, Inc.
AKI No.: 10382**

Prepared By:

Sakhalin Finnie

Sakhalin Finnie
Report Coordinator

Reviewed By:

Shawn Graham

Shawn Graham
Project Manager



EMISSIONS CHARACTERIZATION
AND TESTING SERVICES

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1.0 SUMMARY

1.1 Source Information

Plant Name and Address: Ogden Martin Systems Of Lake, Inc.
3830 Rogers Industrial Park
Okahumpka, Florida 34762

Source Tested: Unit Nos. 1 and 2

Permit ID #: A035-193817

Plant Contact: Cecil Boatwright, Facility Manager

Phone Number: (352) 365-1611

1.2 Testing Firm Information

Firm Name and Address: AirKinetics, Inc.
5932 Bolsa Avenue, Suite 105
Huntington Beach, CA 92649

Firm Contact: Shawn Graham, Project Manager

Phone Number: (714) 373-0998 Ext. 27

Subcontractors: Quanterra Incorporated, West Sacramento, California
Philip Analytical Services, Burlington, Ontario

1.3 Test Information

Test Requested By: Ogden Energy Group, Inc.

Firm Contact: Joe Aldina, Sr. Vice President, Environmental Testing/CEM

Phone Number: (973) 882-4136

Test Objective: Engineering testing to determine mercury emissions and control efficiency.

Test Methods:

EPA 1	Sampling Point Determination
EPA 2	Velocity and Flow Rate
EPA 3	Molecular Weight
EPA 4	Flue Gas Moisture Content
EPA 101A	Mercury
Mod. EPA 101A	Mercury Speciation

Test Dates: March 3 and 4, 1998

1.4 Test Personnel

Test Coordinator: Joe Aldina, Ogden Energy Group, Inc.

AirKinetics Test Personnel:
Shawn Graham, Project Manager
Son Bui, Project Supervisor
Hung Duong, Team Leader
Wayne Johnson, Team Leader
Herbert Dixon, Laboratory Technician

2.0 TEST RESULTS AND DATA PRESENTATION

The results of the testing are summarized in Tables 2-1 and 2-2. Results tabulations are presented in Appendix A. Example calculations are given in Appendix B. Field data are given in Appendix C. Analytical data are provided in Appendix D.

**TABLE 2-1
 UNIT 1 MERCURY TEST RESULTS**

Parameter	Units	Run 1	Run 2	Run 3	Run 4	Run 5
Unit No. 1 Inlet						
Mercury	ug/dscm @ 7% O ₂		1353	1731	1055	564
Unit No. 1 STACK						
Mercury	ug/dscm @ 7% O ₂		67.6	89.8	85.3	83.7
	% Efficiency ^a		95.0	94.8	91.9	85.2
Unit No. 2 Inlet						
Mercury	ug/dscm @ 7% O ₂	50.6	157	129	98.7	
Unit No. 2 STACK						
Mercury	ug/dscm @ 7% O ₂	1.41	11.5	7.57	5.87	
	% Efficiency ^a	97.2	92.7	94.1	94.1	

^a - Efficiency calculated using ug/dscm @ 7% O₂ results.

TABLE 2-2
SPECIATED MERCURY TEST RESULTS

PARAMETER		UNIT 1		UNIT 2	
Mercury	Component	Inlet	Outlet	Inlet	Outlet
Particulate	Front Half Rinse	70	—	32	0.48
Combined	1st & 2nd Impingers (0.1N KCl)	56	32	27	3.3
	3rd Impinger (0.1N KCl)	0.95	0.8	0.017	ND
(Split)	1st & 2nd Impingers (KMnO ₄)	69.0	33.0	36.0	3.4
	3rd Impinger (KMnO ₄)	--	--	0.22	0.056
	Total	125.95	65.80	63.24	6.76
Gaseous	KMnO ₄	ND	ND	0.17	ND
	8N HCl Rinse	3.9	0.16	1.9	0.062
	Total	3.9	0.16	2.07	0.062
Overall Mercury Total		199.85	65.96	97.31	7.30
ug/dscm @ 7% O₂		284	105	107	10.4
Overall % Efficiency		63.0%		90.3%	

3.0 INTRODUCTION

On March 3 and 4, 1998 AirKinetics, Inc. conducted engineering emissions testing for Ogden Energy Group, Inc. at Ogden Martin Systems of Lake, Inc. in Okahumpka, Florida. The objective of the test program was to determine mercury emissions and control efficiency. The testing was conducted on both Unit Nos. 1 and 2. The methods used during this test program were EPA Method 1 for sampling point determination, EPA Method 2 for velocity and flow rate, EPA Method 3 for molecular weight, EPA Method 4 for flue gas moisture content, EPA Method 101A for mercury (Hg), and Modified EPA Method 101A for Hg speciation.

Following is a test log is presented in Table 3-1 which lists the test locations, sampling objectives, sampling methods, test dates, and run numbers for the test program.

TABLE 3-1
 TEST LOG

Sampling Objective	Sampling Method	Test Date	Run Numbers					
Unit No. 1 Inlet								
O ₂ and CO ₂	EPA 3	3/4/98	1-I-M3-1	1-I-M3-2	1-I-M3-3	1-I-M3-4	1-I-M3-5	1-I-M3-6
Hg	EPA 101A		1-I-M101A-1	1-I-M101A-2	1-I-M101A-3	1-I-M101A-4	1-I-M101A-5	
Hg Speciation	Mod. EPA 101A							1-I-MM101A-1
Unit No. 1 Outlet								
O ₂ and CO ₂	EPA 3	3/4/98	1-O-M3-1	1-O-M3-2	1-O-M3-3	1-O-M3-4	1-O-M3-5	1-O-M3-6
Hg	EPA 101A		1-O-M101A-1	1-O-M101A-2	1-O-M101A-3	1-O-M101A-4	1-O-M101A-5	
Hg Speciation	Mod. EPA 101A							1-O-MM101A-1
Unit No. 2 Inlet								
O ₂ and CO ₂	EPA 3	3/3/98	2-I-M3-1	2-I-M3-2	2-I-M3-3	2-I-M3-4	2-I-M3-5	2-I-M3-6
Hg	EPA 101A		2-I-M101A-1	2-I-M101A-2	2-I-M101A-3	2-I-M101A-4	2-I-M101A-5	
Hg Speciation	Mod. EPA 101A							2-I-MM101A-1
Unit No. 2 Outlet								
O ₂ and CO ₂	EPA 3	3/3/98	2-O-M3-1	2-O-M3-2	2-O-M3-3	2-O-M3-4	2-O-M3-5	2-O-M3-6
Hg	EPA 101A		2-O-M101A-1	2-O-M101A-2	2-O-M101A-3	2-O-M101A-4	2-O-M101A-5	
Hg Speciation	Mod. EPA 101A							2-O-MM101A-1

4.0 TEST CRITIQUE

No sampling train leaks were observed during testing. The average sampling rate for each test run was within 10% of isokinetic. A minimum sample volume of 30 standard cubic feet was collected.

A field blank was analyzed with no Hg detected. A reagent blank was analyzed with no Hg detected. A method blank was performed with no Hg detected. A Matrix spike and matrix duplicate were conducted with results within acceptable limits. All mercury analyses were performed in duplicate and the RPD's of the duplicate analyses were within the acceptable limits.

During the final test run on each unit, the EPA Method 101A train was modified to allow for speciation of the elemental and oxidized mercury. The train modification consisted of three extra impingers placed prior to the 10% H₂SO₄ / 4% KMnO₄ impingers. Each impinger contained approximately 100 ml of 0.1N KCl. These impingers were used to capture the oxidized Hg. The elemental Hg was then captured in the 10% H₂SO₄/4% KMnO₄ reagent.

APPENDIX A
RESULTS TABULATION

1.0 UNIT NO. 1

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA
 Test Location: UNIT No. 1 INLET

<u>Run Number</u>	<u>Run Date</u>	<u>Operator</u>
1-I-M101A-2	03/04/98	SON BUI
1-I-M101A-3	03/04/98	SON BUI

		<u>1-I-M101A-2</u>	<u>1-I-M101A-3</u>
	Run Start Time	1010	1145
	Run Stop Time	1116	1254
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.255	0.256
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	0.9647	0.9647
Pbar	Barometric Pressure, Inches Hg	29.90	29.90
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.709	1.615
Vm	Sampled Volume of Source Gas, Dry ACF	44.281	43.073
Vmm	Sampled Volume of Source Gas, Dry ACM	1.25	1.22
tm	Dry Gas Meter Temperature, Degrees F	77.8	79.1
Vmstd	Sampled Volume of Source Gas, Dry SCF	42.085	40.833
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.192	1.156
Vlc	Volume of Condensed Liquid, mL	114.8	110.8
Vwstd	Volume of Water Vapor, SCF	5.403	5.215
%H2O	Moisture Content, Percent by Volume	11.38	11.32
%H2Osat	Saturated Moisture Content, Percent by Volume	100.0	100.0
Mfd	Source Gas Dry Mole Fraction	0.886	0.887
%CO2	Source Gas CO2 Content, Percent by Dry Volume	8.2	8.6
%O2	Source Gas O2 Content, Percent by Dry Volume	11.3	11.1
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.76	29.82
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.43	28.48
Pg	Source Gas Static Pressure, Inches H2O	-2.90	-2.50
Ps	Source Gas Absolute Pressure, Inches Hg	29.69	29.72
ts	Source Gas Temperature, Degrees F	422	419
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.7488	0.6931
vs	Source Gas Velocity, Feet/Second	63.54	60.93
A	Source Cross Sectional Area, Square Inches	3,025	3,025
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	42,142	40,622
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,193	1,150
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	80,088	76,800
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,268	2,175
%I	Average Isokinetic Sampling Rate, Percent	98.6	98.5
Fo	Fuel Factor	1.17	1.14
%EA	Excess Air, Percent	113.5	109.9
Fd	F-Factor, DSCF/Million Btu	9,570	9,570
MMBtu/Hr	Heat Input Rate, Million Btu/Hour	121	119

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>1-I-M101A-2</u>	<u>1-I-M101A-3</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	1113.5	1411.0
ppmvd	Concentration, Parts per Million by Volume Dry	0.112	0.146
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.162	0.208
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.164	0.204
ug/DSCM	Concentration, Micrograms per DSCM	934	1220
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	1353	1731
ug/DSCM@12%CO2	Concentration, ug/DSCM @ 12% CO2	1367	1703
lb/hr	Emission Rate, Pounds per Hour	0.147	0.186
g/sec	Emission Rate, Grams Per Second	0.0186	0.0234
lb/MMBtu	Emission Rate, Pounds per Million Btu	0.00122	0.00155

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA
 Test Location: UNIT No. 1 INLET

<u>Run Number</u>	<u>Run Date</u>	<u>Operator</u>
1-I-M101A-4	03/04/98	SON BUI
1-I-M101A-5	03/04/98	SON BUI

		<u>1-I-M101A-4</u>	<u>1-I-M101A-5</u>
	Run Start Time	1354	1523
	Run Stop Time	1458	1628
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.255	0.256
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	0.9647	0.9647
Pbar	Barometric Pressure, Inches Hg	29.90	29.90
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.718	1.617
Vm	Sampled Volume of Source Gas, Dry ACF	44.930	43.727
Vmm	Sampled Volume of Source Gas, Dry ACM	1.27	1.24
tm	Dry Gas Meter Temperature, Degrees F	81.0	82.6
Vmstd	Sampled Volume of Source Gas, Dry SCF	42.456	41.182
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.202	1.166
Vlc	Volume of Condensed Liquid, mL	112.1	120.3
Vwstd	Volume of Water Vapor, SCF	5.276	5.662
%H2O	Moisture Content, Percent by Volume	11.05	12.09
%H2Osat	Saturated Moisture Content, Percent by Volume	100.0	100.0
Mfd	Source Gas Dry Mole Fraction	0.889	0.879
%CO2	Source Gas CO2 Content, Percent by Dry Volume	8.9	8.4
%O2	Source Gas O2 Content, Percent by Dry Volume	10.9	11.1
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.86	29.79
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.55	28.36
Pg	Source Gas Static Pressure, Inches H2O	-3.00	-2.70
Ps	Source Gas Absolute Pressure, Inches Hg	29.68	29.70
ts	Source Gas Temperature, Degrees F	422	419
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.7472	0.6891
vs	Source Gas Velocity, Feet/Second	63.32	60.91
A	Source Cross Sectional Area, Square Inches	3,025	3,025
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	42,169	40,224
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,194	1,139
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	79,808	76,767
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,260	2,174
%I	Average Isokinetic Sampling Rate, Percent	99.4	100.3
Fo	Fuel Factor	1.12	1.17
%EA	Excess Air, Percent	106.1	109.3
Fd	F-Factor, DSCF/Million Btu	9,570	9,570
MMBtu/Hr	Heat Input Rate, Million Btu/Hour	127	118

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>1-I-M101A-4</u>	<u>1-I-M101A-5</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	912.7	463.4
ppmvd	Concentration, Parts per Million by Volume Dry	0.0910	0.0477
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.127	0.0676
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.123	0.0681
ug/DSCM	Concentration, Micrograms per DSCM	759	397
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	1055	564
ug/DSCM@12%CO2	Concentration, ug/DSCM @ 12% CO2	1024	568
lb/hr	Emission Rate, Pounds per Hour	0.120	0.0599
g/sec	Emission Rate, Grams Per Second	0.0151	0.00754
lb/MMBtu	Emission Rate, Pounds per Million Btu	0.000948	0.000506

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA
 Test Location: UNIT No. 1 OUTLET

<u>Run Number</u>	<u>Run Date</u>	<u>Operator</u>
1-O-M101A-2	3/4/98	WAYNE JOHNSON
1-O-M101A-3	3/4/98	WAYNE JOHNSON

		<u>1-O-M101A-2</u>	<u>1-O-M101A-3</u>
	Run Start Time	1010	1145
	Run Stop Time	1113	1249
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.217	0.217
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	0.9988	0.9988
Pbar	Barometric Pressure, Inches Hg	29.90	29.90
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.195	1.211
Vm	Sampled Volume of Source Gas, Dry ACF	36.355	36.730
Vmm	Sampled Volume of Source Gas, Dry ACM	1.03	1.04
tm	Dry Gas Meter Temperature, Degrees F	73.8	81.5
Vmstd	Sampled Volume of Source Gas, Dry SCF	35.999	35.857
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.019	1.015
Vlc	Volume of Condensed Liquid, mL	133.2	129.4
Vwstd	Volume of Water Vapor, SCF	6.269	6.090
%H2O	Moisture Content, Percent by Volume	14.83	14.52
%H2Osat	Saturated Moisture Content, Percent by Volume	100.0	100.0
Mfd	Source Gas Dry Mole Fraction	0.852	0.855
%CO2	Source Gas CO2 Content, Percent by Dry Volume	8.0	8.0
%O2	Source Gas O2 Content, Percent by Dry Volume	11.6	11.6
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.74	29.74
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.00	28.04
Pg	Source Gas Static Pressure, Inches H2O	-17.60	-17.60
Ps	Source Gas Absolute Pressure, Inches Hg	28.61	28.61
ts	Source Gas Temperature, Degrees F	283	284
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.9609	0.9628
vs	Source Gas Velocity, Feet/Second	67.79	67.88
A	Source Cross Sectional Area, Square Inches	2,627	2,627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	42,944	43,072
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,216	1,220
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	74,206	74,305
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,101	2,104
%I	Average Isokinetic Sampling Rate, Percent	99.2	98.6
Fo	Fuel Factor	1.16	1.16
%EA	Excess Air, Percent	120.5	120.5
Fd	F-Factor, DSCF/Million Btu	9,570	9,570
MMBtu/Hr	Heat Input Rate, Million Btu/Hour	120	120

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>1-O-M101A-2</u>	<u>1-O-M101A-3</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	46.1	61.0
ppmvd	Concentration, Parts per Million by Volume Dry	0.0054	0.00720
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.0081	0.0108
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.0081	0.0108
ug/DSCM	Concentration, Micrograms per DSCM	45.2	60.1
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	67.6	89.8
ug/DSCM@12%CO2	Concentration, ug/DSCM @ 12% CO2	67.8	90.1
lb/hr	Emission Rate, Pounds per Hour	0.00727	0.00969
g/sec	Emission Rate, Grams Per Second	0.000916	0.00122
lb/MMBtu	Emission Rate, Pounds per Million Btu	0.0000607	0.0000807

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA
 Test Location: UNIT No. 1 OUTLET

<u>Run Number</u>	<u>Run Date</u>	<u>Operator</u>
1-O-M101A-4	3/4/98	WAYNE JOHNSON
1-O-M101A-5	3/4/98	WAYNE JOHNSON

		<u>1-O-M101A-4</u>	<u>1-O-M101A-5</u>
	Run Start Time	1354	1522
	Run Stop Time	1457	1626
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.217	0.217
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	0.9988	0.9988
Pbar	Barometric Pressure, Inches Hg	29.90	29.90
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.142	1.188
Vm	Sampled Volume of Source Gas, Dry ACF	35.708	36.530
Vmm	Sampled Volume of Source Gas, Dry ACM	1.01	1.03
tm	Dry Gas Meter Temperature, Degrees F	77.4	81.5
Vmstd	Sampled Volume of Source Gas, Dry SCF	35.115	35.657
Vmstdm	Sampled Volume of Source Gas, Dry SCM	0.994	1.010
Vlc	Volume of Condensed Liquid, mL	128.6	129.8
Vwstd	Volume of Water Vapor, SCF	6.053	6.109
%H2O	Moisture Content, Percent by Volume	14.70	14.63
%H2Osat	Saturated Moisture Content, Percent by Volume	100.0	100.0
Mfd	Source Gas Dry Mole Fraction	0.853	0.854
%CO2	Source Gas CO2 Content, Percent by Dry Volume	7.9	7.8
%O2	Source Gas O2 Content, Percent by Dry Volume	11.6	11.7
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.73	29.72
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.00	28.00
Pg	Source Gas Static Pressure, Inches H2O	-18.30	-16.50
Ps	Source Gas Absolute Pressure, Inches Hg	28.55	28.69
ts	Source Gas Temperature, Degrees F	284	285
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.9144	0.9473
vs	Source Gas Velocity, Feet/Second	66.22	67.31
A	Source Cross Sectional Area, Square Inches	2,627	2,627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	41,900	42,743
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,186	1,210
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	72,478	73,672
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,052	2,086
%I	Average Isokinetic Sampling Rate, Percent	99.2	98.8
Fo	Fuel Factor	1.18	1.18
%EA	Excess Air, Percent	120.2	122.5
Fd	F-Factor, DSCF/Million Btu	9,570	9,570
MMBtu/Hr	Heat Input Rate, Million Btu/Hour	117	118

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>1-O-M101A-4</u>	<u>1-O-M101A-5</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	56.7	56.0
ppmvd	Concentration, Parts per Million by Volume Dry	0.00684	0.00665
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.0102	0.0100
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.0104	0.0102
ug/DSCM	Concentration, Micrograms per DSCM	57.1	55.4
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	85.3	83.7
ug/DSCM@12%CO2	Concentration, ug/DSCM @ 12% CO2	86.7	85.3
lb/hr	Emission Rate, Pounds per Hour	0.00896	0.00887
g/sec	Emission Rate, Grams Per Second	0.00113	0.00112
lb/MMBtu	Emission Rate, Pounds per Million Btu	0.0000766	0.0000752

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA

Test Location: UNIT No. 1

<u>Run Number</u>	<u>Run Date</u>	<u>Operator</u>
1-I-MM101A-1	03/04/98	SON BUI
1-O-MM101A-1	03/04/98	WAYNE JOHNSON

		<u>1-I-MM101A-1</u>	<u>1-O-MM101A-1</u>
	Run Start Time	1658	1658
	Run Stop Time	1803	1801
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.255	0.217
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	0.9647	0.9988
Pbar	Barometric Pressure, Inches Hg	29.9	29.9
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.63	1.17
Vm	Sampled Volume of Source Gas, Dry ACF	43.733	36.476
Vmm	Sampled Volume of Source Gas, Dry ACM	1.238	1.033
tm	Dry Gas Meter Temperature, Degrees F	84.0	86.2
Vmstd	Sampled Volume of Source Gas, Dry SCF	41.085	35.296
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.163	0.999
Vlc	Volume of Condensed Liquid, mL	138.7	148.9
Vwstd	Volume of Water Vapor, SCF	6.528	7.008
%H2O	Moisture Content, Percent by Volume	13.7	16.6
%H2Osat	Saturated Moisture Content, Percent by Volume	100	100
Mfd	Source Gas Dry Mole Fraction	0.863	0.834
%CO2	Source Gas CO2 Content, Percent by Dry Volume	7.9	7.6
%O2	Source Gas O2 Content, Percent by Dry Volume	12.5	12.2
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.8	29.7
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.2	27.8
Pg	Source Gas Static Pressure, Inches H2O	-2.60	-18.5
Ps	Source Gas Absolute Pressure, Inches Hg	29.7	28.5
ts	Source Gas Temperature, Degrees F	421.8	284.2
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.706	0.921
vs	Source Gas Velocity, Feet/Second	61.9	66.8
A	Source Cross Sectional Area, Square Inches	3,025	2,627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	40,058	41,278
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,134	1,169
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	78,081	73,104
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,211	2,070
%I	Average Isokinetic Sampling Rate, Percent	101	101
Fo	Fuel Factor	1.06	1.14

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>1-I-MM101A-1</u>	<u>1-O-MM101A-1</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	199.9	66.0
ppmvd	Concentration, Parts per Million by Volume Dr	0.0206	0.0079
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.0341	0.0126
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.0313	0.0125
ug/DSCM	Concentration, Micrograms per DSCM	172	66.0
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	284	105
ug/DSCM@12%CO	Concentration, ug/DSCM @ 12% CO2	261	104
lb/hr	Emission Rate, Pounds per Hour	0.0258	0.0102
g/sec	Emission Rate, Grams Per Second	0.00325	0.00129

* - The catch weight was corrected for the reagent blank analytical results.

APPENDIX A
RESULTS TABULATION

2.0 UNIT NO. 2

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA
 Test Location: UNIT No. 2 INLET

Run Number	Run Date	Operator
2-I-M101A-1	03/03/98	SON BUI
2-I-M101A-2	03/03/98	SON BUI

		<u>2-I-M101A-1</u>	<u>2-I-M101A-2</u>
	Run Start Time	922	1205
	Run Stop Time	1036	1311
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.255	0.253
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	0.9647	0.9647
Pbar	Barometric Pressure, Inches Hg	29.80	29.80
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.633	1.634
Vm	Sampled Volume of Source Gas, Dry ACF	43.254	43.331
Vmm	Sampled Volume of Source Gas, Dry ACM	1.22	1.23
tm	Dry Gas Meter Temperature, Degrees F	77.5	78.5
Vmstd	Sampled Volume of Source Gas, Dry SCF	40.993	40.987
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.161	1.161
Vlc	Volume of Condensed Liquid, mL	139.2	126.8
Vwstd	Volume of Water Vapor, SCF	6.551	5.968
%H2O	Moisture Content, Percent by Volume	13.78	12.71
%H2Osat	Saturated Moisture Content, Percent by Volume	100.0	100.0
Mfd	Source Gas Dry Mole Fraction	0.862	0.873
%CO2	Source Gas CO2 Content, Percent by Dry Volume	8.5	8.7
%O2	Source Gas O2 Content, Percent by Dry Volume	12.1	10.9
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.84	29.83
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.21	28.32
Pg	Source Gas Static Pressure, Inches H2O	-2.40	-2.40
Ps	Source Gas Absolute Pressure, Inches Hg	29.62	29.62
ts	Source Gas Temperature, Degrees F	454	471
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.7399	0.8006
vs	Source Gas Velocity, Feet/Second	64.61	67.70
A	Source Cross Sectional Area, Square Inches	3,025	3,025
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	40,145	41,803
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,137	1,184
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	81,436	85,328
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,306	2,416
%I	Average Isokinetic Sampling Rate, Percent	100.8	98.3
Fo	Fuel Factor	1.04	1.15
%EA	Excess Air, Percent	136.5	105.6
Fd	F-Factor, DSCF/Million Btu	9,570	9,570
MMBtu/Hr	Heat Input Rate, Million Btu/Hour	106	125

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>2-I-M101A-1</u>	<u>2-I-M101A-2</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	37.2	131.1
ppmvd	Concentration, Parts per Million by Volume Dry	0.00384	0.0135
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.00607	0.0188
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.00543	0.0187
ug/DSCM	Concentration, Micrograms per DSCM	32.0	113
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	50.6	157
ug/DSCM@12%CO2	Concentration, ug/DSCM @ 12% CO2	45.2	156
lb/hr	Emission Rate, Pounds per Hour	0.00482	0.0177
g/sec	Emission Rate, Grams Per Second	0.000607	0.00223
lb/MMBtu	Emission Rate, Pounds per Million Btu	0.0000455	0.000141

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA
 Test Location: UNIT No. 2 INLET

<u>Run Number</u>	<u>Run Date</u>	<u>Operator</u>
2-I-M101A-3	03/03/98	SON BUI
2-I-M101A-4	03/03/98	SON BUI

		<u>2-I-M101A-3</u>	<u>2-I-M101A-4</u>
	Run Start Time	1344	1518
	Run Stop Time	1452	1623
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.255	0.255
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	0.9647	0.9647
Pbar	Barometric Pressure, Inches Hg	29.80	29.80
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.529	1.750
Vm	Sampled Volume of Source Gas, Dry ACF	42.000	45.369
Vmm	Sampled Volume of Source Gas, Dry ACM	1.19	1.28
tm	Dry Gas Meter Temperature, Degrees F	81.2	82.4
Vmstd	Sampled Volume of Source Gas, Dry SCF	39.519	42.617
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.119	1.207
Vlc	Volume of Condensed Liquid, mL	132.6	148.7
Vwstd	Volume of Water Vapor, SCF	6.241	6.999
%H2O	Moisture Content, Percent by Volume	13.64	14.11
%H2Osat	Saturated Moisture Content, Percent by Volume	100.0	100.0
Mfd	Source Gas Dry Mole Fraction	0.864	0.859
%CO2	Source Gas CO2 Content, Percent by Dry Volume	8.9	9.4
%O2	Source Gas O2 Content, Percent by Dry Volume	11.0	10.2
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.86	29.91
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.25	28.23
Pg	Source Gas Static Pressure, Inches H2O	-2.60	-2.60
Ps	Source Gas Absolute Pressure, Inches Hg	29.61	29.61
ts	Source Gas Temperature, Degrees F	459	475
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.7119	0.8289
vs	Source Gas Velocity, Feet/Second	63.50	69.17
A	Source Cross Sectional Area, Square Inches	3,025	3,025
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	39,319	41,825
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,113	1,184
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	80,039	87,177
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,266	2,469
%I	Average Isokinetic Sampling Rate, Percent	99.2	100.6
Fo	Fuel Factor	1.11	1.14
%EA	Excess Air, Percent	108.4	92.5
Fd	F-Factor, DSCF/Million Btu	9,570	9,570
MMBtu/Hr	Heat Input Rate, Million Btu/Hour	117	134

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>2-I-M101A-3</u>	<u>2-I-M101A-4</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	102.6	91.7
ppmvd	Concentration, Parts per Million by Volume Dry	0.0110	0.00911
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.0154	0.0118
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.0148	0.0116
ug/DSCM	Concentration, Micrograms per DSCM	91.7	76.0
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	129	98.7
ug/DSCM@12%CO2	Concentration, ug/DSCM @ 12% CO2	124	97.0
lb/hr	Emission Rate, Pounds per Hour	0.0135	0.0119
g/sec	Emission Rate, Grams Per Second	0.00170	0.00150
lb/MMBtu	Emission Rate, Pounds per Million Btu	0.000116	0.0000887

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA
 Test Location: UNIT No. 2 OUTLET

<u>Run Number</u>	<u>Run Date</u>	<u>Operator</u>
2-O-M101A-1	3/3/98	WAYNE JOHNSON
2-O-M101A-2	3/3/98	WAYNE JOHNSON

	<u>2-O-M101A-1</u>	<u>2-O-M101A-2</u>	
Run Start Time	922	1205	
Run Stop Time	1028	1319	
Net Sampling/Traversing Points	24	24	
Net Run Time, Minutes	60	60	
Dia	Nozzle Diameter, Inches	0.217	0.217
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	0.9988	0.9988
Pbar	Barometric Pressure, Inches Hg	29.80	29.80
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.335	1.261
Vm	Sampled Volume of Source Gas, Dry ACF	38.497	37.180
Vmm	Sampled Volume of Source Gas, Dry ACM	1.09	1.05
tm	Dry Gas Meter Temperature, Degrees F	65.4	69.8
Vmstd	Sampled Volume of Source Gas, Dry SCF	38.612	36.976
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.093	1.047
Vlc	Volume of Condensed Liquid, mL	169.7	140.6
Vwstd	Volume of Water Vapor, SCF	7.987	6.617
%H2O	Moisture Content, Percent by Volume	17.14	15.18
%H2Osat	Saturated Moisture Content, Percent by Volume	100.0	100.0
Mfd	Source Gas Dry Mole Fraction	0.829	0.848
%CO2	Source Gas CO2 Content, Percent by Dry Volume	5.9	5.2
%O2	Source Gas O2 Content, Percent by Dry Volume	13.8	14.4
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.50	29.41
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	27.53	27.68
Pg	Source Gas Static Pressure, Inches H2O	-16.10	-16.40
Ps	Source Gas Absolute Pressure, Inches Hg	28.62	28.59
ts	Source Gas Temperature, Degrees F	282	280
Delta-p	Source Gas Average Velocity Head, Inches H2O	1.0779	1.0125
vs	Source Gas Velocity, Feet/Second	72.34	69.89
A	Source Cross Sectional Area, Square Inches	2, 627	2, 627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	44, 680	44, 228
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1, 265	1, 252
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	79, 184	76, 502
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2, 242	2, 166
%I	Average Isokinetic Sampling Rate, Percent	102.3	99.0
Fo	Fuel Factor	1.20	1.25
%EA	Excess Air, Percent	186.5	211.0
Fd	F-Factor, DSCF/Million Btu	9, 570	9, 570
MMBtu/Hr	Heat Input Rate, Million Btu/Hour	95	86

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) — 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>2-0-M101A-1</u>	<u>2-0-M101A-2</u>
	<u>Mercury</u>		
Fwt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	0.79	5.6
ppmvd	Concentration, Parts per Million by Volume Dry	0.0000866	0.000645
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.000170	0.001379
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.000176	0.001488
ug/DSCM	Concentration, Micrograms per DSCM	0.723	5.38
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	1.41	11.50
ug/DSCM@12%CO2	Concentration, ug/DSCM @ 12% CO2	1.47	12.41
lb/hr	Emission Rate, Pounds per Hour	0.000121	0.000891
g/sec	Emission Rate, Grams Per Second	0.0000152	0.000112
lb/MMBtu	Emission Rate, Pounds per Million Btu	0.00000127	0.00001033

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA
 Test Location: UNIT No. 2 OUTLET

<u>Run Number</u>	<u>Run Date</u>	<u>Operator</u>
2-O-M101A-3	3/3/98	WAYNE JOHNSON
2-O-M101A-4	3/3/98	WAYNE JOHNSON

		<u>2-O-M101A-3</u>	<u>2-O-M101A-4</u>
	Run Start Time	1344	1518
	Run Stop Time	1447	1622
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.217	0.217
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	0.9988	0.9988
Pbar	Barometric Pressure, Inches Hg	29.80	29.80
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.253	1.300
Vm	Sampled Volume of Source Gas, Dry ACF	37.095	37.602
Vmm	Sampled Volume of Source Gas, Dry ACM	1.05	1.06
tm	Dry Gas Meter Temperature, Degrees F	69.2	70.8
Vmstd	Sampled Volume of Source Gas, Dry SCF	36.931	37.329
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.046	1.057
Vlc	Volume of Condensed Liquid, mL	157.5	162.3
Vwstd	Volume of Water Vapor, SCF	7.413	7.639
%H2O	Moisture Content, Percent by Volume	16.72	16.99
%H2Osat	Saturated Moisture Content, Percent by Volume	100.0	100.0
Mfd	Source Gas Dry Mole Fraction	0.833	0.830
%CO2	Source Gas CO2 Content, Percent by Dry Volume	8.5	8.7
%O2	Source Gas O2 Content, Percent by Dry Volume	11.1	11.0
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.80	29.83
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	27.83	27.82
Pg	Source Gas Static Pressure, Inches H2O	-14.60	-16.60
Ps	Source Gas Absolute Pressure, Inches Hg	28.73	28.58
ts	Source Gas Temperature, Degrees F	281	282
Delta-p	Source Gas Average Velocity Head, Inches H2O	1.0027	1.0431
vs	Source Gas Velocity, Feet/Second	69.23	70.86
A	Source Cross Sectional Area, Square Inches	2,627	2,627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	43,169	43,750
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,222	1,239
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	75,783	77,564
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,146	2,196
%I	Average Isokinetic Sampling Rate, Percent	101.3	101.0
Fo	Fuel Factor	1.15	1.14
%EA	Excess Air, Percent	109.6	107.9
Fd	F-Factor, DSCF/Million Btu	9,570	9,570
MMBtu/Hr	Heat Input Rate, Million Btu/Hour	127	130

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes.

FIELD DATA AND RESULTS TABULATION

		<u>2-O-M101A-3</u>	<u>2-O-M101A-4</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	5.6	6.2
ppmvd	Concentration, Parts per Million by Volume Dry	0.000640	0.000703
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.000907	0.000988
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.000903	0.000970
ug/DSCM	Concentration, Micrograms per DSCM	5.33	5.87
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	7.57	8.24
ug/DSCM@12%CO2	Concentration, ug/DSCM @ 12% CO2	7.53	8.09
lb/hr	Emission Rate, Pounds per Hour	0.000862	0.000961
g/sec	Emission Rate, Grams Per Second	0.000109	0.000121
lb/MMBtu	Emission Rate, Pounds per Million Btu	0.00000680	0.00000740

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA

Test Location: UNIT No. 2

Run Number	Run Date	Operator
2-I-MM101A-1	03/03/98	SON BUI
2-O-MM101A-1	03/03/98	WAYNE JOHNSON

		<u>2-I-MM101A-1</u>	<u>2-O-MM101A-1</u>
	Run Start Time	1655	1655
	Run Stop Time	1803	1755
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.256	0.217
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	0.9647	0.9988
Pbar	Barometric Pressure, Inches Hg	29.8	29.8
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.64	1.28
Vm	Sampled Volume of Source Gas, Dry ACF	43.852	37.592
Vmm	Sampled Volume of Source Gas, Dry ACM	1.242	1.064
tm	Dry Gas Meter Temperature, Degrees F	76.6	70.0
Vmstd	Sampled Volume of Source Gas, Dry SCF	41.624	37.373
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.179	1.058
Vlc	Volume of Condensed Liquid, mL	140.0	146.6
Vwstd	Volume of Water Vapor, SCF	6.589	6.900
%H2O	Moisture Content, Percent by Volume	13.7	15.6
%H2Osat	Saturated Moisture Content, Percent by Volume	100	100
Mfd	Source Gas Dry Mole Fraction	0.863	0.844
%CO2	Source Gas CO2 Content, Percent by Dry Volume	9.4	8.3
%O2	Source Gas O2 Content, Percent by Dry Volume	10.2	11.7
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.9	29.8
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.3	28.0
Pg	Source Gas Static Pressure, Inches H2O	-2.50	-16.1
Ps	Source Gas Absolute Pressure, Inches Hg	29.6	28.6
ts	Source Gas Temperature, Degrees F	473.6	284.0
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.768	1.040
vs	Source Gas Velocity, Feet/Second	66.4	70.6
A	Source Cross Sectional Area, Square Inches	3,025	2,627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	40,468	44,292
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,146	1,254
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	83,734	77,302
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,371	2,189
%I	Average Isokinetic Sampling Rate, Percent	101	99.9
Fo	Fuel Factor	1.14	1.11

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>2-I-MM101A-1</u>	<u>2-O-MM101A-1</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	97.31	7.30
ppmvd	Concentration, Parts per Million by Volume Dr	0.0099	0.000827
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.0129	0.00125
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.0126	0.00120
ug/DSCM	Concentration, Micrograms per DSCM	83	6.90
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	107	10.4
ug/DSCM@12%CO	Concentration, ug/DSCM @ 12% CO2	105	10.0
lb/hr	Emission Rate, Pounds per Hour	0.0125	0.00114
g/sec	Emission Rate, Grams Per Second	0.00158	0.000144

* - The catch weight was corrected for the reagent blank analytical results.

APPENDIX B
EXAMPLE CALCULATIONS

FIELD DATA AND RESULTS TABULATION

EXAMPLE CALCULATIONS, RUN 1-I-M101A-2

SAMPLED VOLUME OF SOURCE GAS, DRY ACTUAL CUBIC FEET

$$\begin{aligned} V_{mm} &= V_m * 0.028317 \\ &= 44.281 * 0.028317 \\ &= 1.25 \end{aligned}$$

SAMPLED VOLUME OF SOURCE GAS, DRY STANDARD CUBIC FEET

$$\begin{aligned} V_{mstd} &= [(T_{std} + 460)/P_{std}] * Y * V_m * (P_{bar} + \Delta H/13.6) / (460 + t_m) \\ &= [(68 + 460)/29.92] * 0.9647 * 44.281 * (29.90 + 1.71/13.6) / (460 + 78) \\ &= 42.085 \end{aligned}$$

SAMPLED VOLUME OF SOURCE GAS, DRY STANDARD CUBIC METER

$$\begin{aligned} V_{mstdm} &= V_{mstd} * 0.028317 \\ &= 42.085 * 0.028317 \\ &= 1.192 \end{aligned}$$

VOLUME OF WATER VAPOR, STANDARD CUBIC FEET

$$\begin{aligned} V_{wstd} &= 0.002667 * [(T_{std} + 460) / P_{std}] * V_{lc} \\ &= 0.002667 * [(68 + 460) / 29.92] * 114.8 \\ &= 5.403 \end{aligned}$$

MOISTURE CONTENT, PERCENT BY VOLUME

$$\begin{aligned} \%H_2O &= V_{wstd} / (V_{wstd} + V_{mstd}) \\ &= 5.403 / (5.403 + 42.085) \\ &= 11.38 \end{aligned}$$

DRY MOLE FRACTION, LB-MOLE/LB-MOLE

$$\begin{aligned} M_{fd} &= 1 - \%H_2O/100 \\ &= 1 - 11.38/100 \\ &= 0.886 \end{aligned}$$

DRY MOLECULAR WEIGHT, LB/LB-MOLE

$$\begin{aligned} M_d &= 44 * (\%CO_2/100) + 32 * (\%O_2/100) + 28 * \{[100 - (\%CO_2 + \%O_2)]/100\} \\ &= 44 * (8.2/100) + 32 * (11.3/100) + 28 * \{[100 - (8.2 + 11.3)]/100\} \\ &= 29.76 \end{aligned}$$

WET MOLECULAR WEIGHT, LB/LB-MOLE

$$\begin{aligned} M_s &= M_d * M_{fd} + 18.0 * \%H_2O/100 \\ &= 29.76 * 0.886 + 18.0 * 11.38/100 \\ &= 28.43 \end{aligned}$$

ABSOLUTE PRESSURE, INCHES OF MERCURY

$$\begin{aligned} P_s &= P_{bar} + P_g/13.6 \\ &= 29.90 + -2.90/13.6 \\ &= 29.69 \end{aligned}$$

VELOCITY, FEET PER SECOND

$$\begin{aligned} v_s &= 85.49 * C_p * \text{SQRT}[\Delta p * (460 + t_s) / P_s / M_s] \\ &= 85.49 * 0.84 * \text{SQRT}[0.7488 * (460 + 422) / 29.69 / 28.43] \\ &= 63.54 \end{aligned}$$

FIELD DATA AND RESULTS TABULATION

VOLUMETRIC FLOW RATE, DRY STANDARD CUBIC FEET PER MINUTE

$$\begin{aligned} Q_{sd} &= (60/144) * M_{fd} * v_s * A * (T_{std} + 460)/(t_s + 460) * (P_s/P_{std}) \\ &= (60/144) * 0.886 * 63.54 * 3025 * (68 + 460)/(422 + 460) * (29.69/29.92) \\ &= 42142 \end{aligned}$$

VOLUMETRIC FLOW RATE, DRY STANDARD CUBIC METER PER MINUTE

$$\begin{aligned} Q_{msd} &= Q_{sd} * 0.028317 \\ &= 42142 * 0.028317 \\ &= 1193 \end{aligned}$$

VOLUMETRIC FLOW RATE, ACTUAL CUBIC FEET PER MINUTE

$$\begin{aligned} Q_{aw} &= (60/144) * v_s * A \\ &= (60/144) * 63.54 * 3025 \\ &= 80088 \end{aligned}$$

VOLUMETRIC FLOW RATE, ACTUAL CUBIC METER PER MINUTE

$$\begin{aligned} Q_{maw} &= Q_{aw} * 0.028317 \\ &= 80088 * 0.028317 \\ &= 2268 \end{aligned}$$

ISOKINETIC SAMPLING RATE, PERCENT

$$\begin{aligned} \%I &= P_{std}/(T_{std} + 460) * (100/60) * V_{mstd} * (t_s + 460) / [P_s * v_s * M_{fd} * \theta * (\pi * \text{Dia} * \text{Dia} / 576)] \\ &= 29.92 / (68 + 460) * (100/60) * 42.085 * (422 + 460) / [29.69 * 63.54 * 0.886 * 60.00 * (\pi * 0.255 * 0.255 / 576)] \\ &= 98.6 \end{aligned}$$

FUEL FACTOR

$$\begin{aligned} F_o &= (20.9 - \%O_2) / 20.9 \\ &= (20.9 - 11.3) / 20.9 \\ &= 1.171 \end{aligned}$$

FIELD DATA AND RESULTS TABULATION

MERCURY CONCENTRATION, PARTS PER MILLION BY VOLUME DRY

$$\begin{aligned}\text{ppmvd} &= (\text{Catch/Conversion}) * 385.3 * 1,000,000 / 453.592 / \text{FWt} / \text{Vmstd} * (460 + \text{Tstd}) / 528 \\ &= (1113.5/1000000) * 385.3 * 1,000,000 / 453.592 / 200.59 / 42.085 * (460 + 68) / 528 \\ &= 0.11204\end{aligned}$$

MERCURY CONCENTRATION, PARTS PER MILLION BY VOLUME DRY @ 7% O2

$$\begin{aligned}\text{ppm@7\%O2} &= \text{ppmvd} * (20.9 - 7) / (20.9 - \%O2) \\ &= 0.1120 * (20.9 - 7) / (20.9 - 11.3) \\ &= 0.16223\end{aligned}$$

MERCURY CONCENTRATION, PARTS PER MILLION BY VOLUME DRY @ 12% CO2

$$\begin{aligned}\text{ppm@12\%CO2} &= \text{ppmvd} * 12 / \%CO2 \\ &= 0.1120 * 12 / 8.2 \\ &= 0.16397\end{aligned}$$

MERCURY CONCENTRATION, MICROGRAMS PER DRY STANDARD CUBIC METER

$$\begin{aligned}\text{ug/DSCM} &= (\text{Catch/Conversion}) * 1,000,000 / \text{Vmstdm} \\ &= (1114/1000000) * 1,000,000 / 1.192 \\ &= 934.4\end{aligned}$$

MERCURY CONCENTRATION, MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2

$$\begin{aligned}\text{ug/DSCM@7\%O2} &= \text{ug/DSCM} * (20.9 - 7) / (20.9 - \%O2) \\ &= (934 * 1,000,000 / 1.192 * (20.9 - 7) / (20.9 - 11.3)) \\ &= 1352.9\end{aligned}$$

MERCURY CONCENTRATION, NANOGRAMS PER DRY STANDARD CUBIC METER @ 12% CO2

$$\begin{aligned}\text{ug/DSCM@12\%CO2} &= \text{ug/DSCM} * (12 / \%CO2) \\ &= (934 * (12/8.2)) \\ &= 1367.4\end{aligned}$$

MERCURY EMISSION RATE, POUNDS PER HOUR

$$\begin{aligned}\text{lb/hr} &= 60 * (\text{Catch/Conversion}) * \text{Qsd} / 453.592 / \text{Vmstd} \\ &= 60 * (1114/1000000) * 42142 / 453.592 / 42.085 \\ &= 0.14749\end{aligned}$$

MERCURY EMISSION RATE, GRAMS PER SECOND

$$\begin{aligned}\text{g/sec} &= (\text{Catch/Conversion}) * \text{Qsd} / 60 / \text{Vmstd} \\ &= 1113.50/1000000 * 42142 / 60 / 42.085 \\ &= 0.018583\end{aligned}$$

APPENDIX C

FIELD DATA

1.0 UNIT NO. 1

a. INLET

METHOD 3 (ORSAT) FIELD DATA

Client OGDEN ENERGY GROUP
 Plant Name OMS LAKE
 City/State OKLAHOMA, FL
 Sampling Location UNIT No. 1 INLET

Job No. 10382
 Fuel Type MUNI WASTE

Run/Sample No. <u>① I-M101A/m3-1</u> Date <u>3/4/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
0835	1000	8.0	19.4	—	11.4	—	
1	1015	8.0	19.6	—	11.6	—	
0940	1022	8.0	19.5	—	11.5	—	
Avg.		8.0	Avg.		11.5	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B203</u>		F _o _____			

Run/Sample No. <u>1-I-m101A/m3-2</u> Date <u>3/4/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1010	1200	8.1	19.4	—	11.3	—	
1	1208	8.2	19.5	—	11.3	—	
1118	1216	8.2	19.5	—	11.3	—	
Avg.		8.2	Avg.		11.3	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B202</u>		F _o _____			

Run/Sample No. <u>1-I-m3-3</u> Date <u>3/4/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1145	1300	8.5	19.6	—	11.1	—	
1	1307	8.7	19.8	—	11.1	—	
1254	1318	8.7	19.8	—	11.1	—	
Avg.		8.6	Avg.		11.1	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B201</u>		F _o _____			<u>6</u> <u>2</u>

METHOD 3 (ORSAT) FIELD DATA

Client OGDEN ENERGY GROUP
 Plant Name OMS LAKE
 City/State OKLAHOMA, FL
 Sampling Location UNIT NO. 1 INLET

Job No. 10382
 Fuel Type MUNI WASTE

Run/Sample No. <u>1-I-M3-4</u> Date <u>3/4/98</u> Leak ✓ OK? <input checked="" type="checkbox"/>							Operator
							<u>SCC</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1354	1512	8.8	19.8	—	10.8	—	
1	1520	9.0	19.9	—	10.9	—	
1458	1528	9.0	19.9	—	10.9	—	
Avg.		8.9	Avg.		10.9	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B203</u>			F ₀ _____		

Run/Sample No. <u>1-I-M3-5</u> Date <u>3/4/98</u> Leak ✓ OK? <input checked="" type="checkbox"/>							Operator
							<u>SCC</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1523	1712	8.3	19.4	—	11.1	—	
1	1720	8.4	19.5	—	11.1	—	
1620	1728	8.4	19.5	—	11.1	—	
Avg.		8.4	Avg.		11.1	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B148</u>			F ₀ _____		

Run/Sample No. <u>1-I-M3-6</u> Date <u>3/4/98</u> Leak ✓ OK? <input checked="" type="checkbox"/>							Operator
							<u>SCC</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1658	1900	7.9	20.4	—	12.5	—	
1	1910	7.9	20.4	—	12.5	—	
1803	1920	8.0	20.5	—	12.5	—	
Avg.		7.9	Avg.		12.5	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B201</u>			F ₀ _____		

ABO

SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: DODEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORAHAMOKA, FL JOB NO.: 10382
 SAMPLE LOCATION: Unit 1 SDA Inlet RUN NO.: 1-I-M101A-1
 BAR. PRESS., IN. HG: 29.9 STATIC PRESSURE, IN. H₂O: -3.0 DATE: 3/4/98
 LEAK ✓ VAC., IN. HG: 15 10 RUN TIME: 0835 - 0940
 LEAK RATE, CFM: 0.001 see test log TEST PERSONS: STB, HDD

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@				XAD	WT.	
PITOT	✓	✓	<u>N20</u>	<u>0.9647</u>	<u>1.83</u>					<u>NA</u>	
TC	✓	✓	PITOT ID <u>PT-12</u>	Cp <u>0.84</u>	METER TEMP. <u>70</u>						
NOZZLE	✓	✓	TC READOUT <u>F107</u>	TC <u>62</u>	EST. % H ₂ O <u>12</u>						
ORSAT	✓	NA	NOZZLE NO. <u>GN2007</u>	DIA. <u>0.256</u>	"C" FACTOR <u>0.852</u>						
			SAMPLE BOX <u>08</u>	REAGNT. <u>217</u>	STACK TEMP. <u>450</u>						
			UMBILICAL <u>U10</u>		REF DELTA-P <u>0.831</u>						
			ORSAT PUMP <u>OR-2</u>	BAG <u>203-A</u>	"K" FACTOR <u>2.213</u>						

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	C-8	0	623.500	0.87	57	405	1.98	1.977	2	248	41	235
2	7	2.5	625.46	0.87	57	400	1.98	1.977	2	260	41	238
3	6	5	627.43	0.83	58	400	1.90	1.896	2	259	42	240
	5	7.5	629.29	0.80	61	398	1.84	1.843	2	250	42	243
	4	10	631.10	0.80	62	398	1.85	1.847	2	250	42	245
6	3	12.5	632.98	0.75	64	391	1.75	1.749	3	250	43	248
7	2	15	634.88	0.68	66	388	1.60	1.598	3	252	44	250
8	1	17.5	636.61	0.62	68	381	1.48	1.475	3	255	45	250
9	B-8	20/0	638.321	0.83	68	396	1.94	1.941	3	240	47	245
10	7	2.5	640.31	0.80	70	399	1.87	1.869	3	242	47	248
11	6	5	642.26	0.70	71	396	1.65	1.645	3	246	48	250
12	5	7.5	644.10	0.65	72	394	1.54	1.535	3	248	48	248
13	4	10	645.87	0.58	73	390	1.38	1.379	3	253	49	250
14	3	12.5	647.56	0.60	74	383	1.44	1.441	3	254	50	249
15	2	15	649.28	0.62	75	385	1.49	1.489	3	256	50	250
16	1	17.5	651.01	0.55	76	380	1.33	1.331	3	258	51	250
17	A-8	40/0	652.656	0.73	76	405	1.72	1.716	3	243	52	245
18	7	2.5	654.56	0.82	76	412	1.91	1.910	4	245	52	250
19	6	5	656.53	0.75	77	411	1.75	1.751	4	245	52	250
20	5	7.5	658.44	0.76	78	408	1.79	1.785	4	243	53	250
21	4	10	660.37	0.73	79	403	1.73	1.727	4	241	53	248
22	3	12.5	662.27	0.75	79	400	1.78	1.781	4	245	54	250
23	2	15	664.18	0.64	80	395	1.53	1.532	4	248	54	250
	1	17.5	665.95	0.72	80	400	1.71	1.714	4	252	55	250
		60	667.848									

FINAL REVIEWER SLC

60 44.150 0.7242 70.7 396.6 1.7058
44.348

SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, OK JOB NO.: 10382
 SAMPLE LOCATION: Unit 1 SDA Inlet RUN NO.: 1-I-M101A-2
 BAR. PRESS., IN. HG: 29.9 STATIC PRESSURE, IN. H₂O: -2.90 DATE: 3/4/98
 LEAK ✓ VAC., IN. HG: 15 10 RUN TIME: 1010 - 1116
 LEAK RATE, CFM: 0.000 0.000 TEST PERSONS: STP, HDD

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS		NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@		XAD	WT.	
PITOT	✓	✓	<u>N30</u>	<u>0.9647</u>	<u>1.83</u>			<u>NA</u>	
TC	✓	✓	PITOT ID <u>PT15</u>	Cp <u>0.84</u>	METER TEMP. <u>75</u>				
NOZZLE	✓	✓	TC READOUT <u>F107</u>	TC	EST. % H ₂ O <u>12</u>				
ORSAT	✓	NA	NOZZLE NO. <u>GN2003</u>	DIA. <u>0.255</u>	"C" FACTOR <u>0.850</u>				
			SAMPLE BOX <u>07</u>	REAGNT. <u>217</u>	STACK TEMP. <u>400</u>				
			UMBILICAL <u>U10</u>		REF DELTA-P <u>0.799</u>				
			ORSAT PUMP <u>OR 2</u>	BAG <u>202-A</u>	"K" FACTOR <u>2.302</u>				

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-8	0	669.500	0.83	71	420	1.87	1.872	2	240	49	240
2	7	2.5	671.49	0.77	71	422	1.73	1.729	2	245	48	240
3	6	5	673.32	0.80	71	420	1.80	1.801	2	255	48	243
	5	7.5	675.19	0.72	72	418	1.63	1.627	2	255	49	245
	4	10	677.00	0.70	73	414	1.59	1.593	3	256	49	247
6	3	12.5	678.75	0.73	74	414	1.66	1.664	3	256	50	250
7	2	15	680.55	0.76	75	419	1.73	1.726	3	258	51	250
8	1	17.5	682.40	0.73	76	421	1.66	1.657	4	258	51	248
9	B-8	20/0	684.224	0.90	76	424	2.04	2.036	5	250	52	250
10	7	2.5	686.28	0.92	77	427	2.08	2.076	5	255	53	250
11	6	5	688.35	0.85	79	429	1.92	1.921	5	260	53	246
12	5	7.5	690.32	0.75	80	429	1.70	1.699	5	265	54	249
13	4	10	692.15	0.70	80	428	1.59	1.588	5	268	55	250
14	3	12.5	693.93	0.72	81	426	1.64	1.641	6	266	55	250
15	2	15	695.72	0.75	81	431	1.70	1.700	6	265	56	250
16	1	17.5	697.53	0.70	81	429	1.59	1.590	6	266	57	245
17	C-8	40/0	699.320	0.90	79	425	2.05	2.046	7	251	57	248
18	7	2.5	701.35	0.83	80	426	1.89	1.886	7	256	58	250
19	6	5	703.32	0.80	81	424	1.83	1.826	8	258	58	250
20	5	7.5	705.20	0.64	81	421	1.47	1.466	8	250	59	250
21	4	10	706.93	0.62	82	419	1.43	1.427	8	256	59	248
22	3	12.5	708.65	0.65	82	418	1.50	1.498	8	257	60	246
23	2	15	710.38	0.63	82	417	1.45	1.454	8	257	60	248
	1	17.5	712.08	0.63	83	415	1.46	1.460	8	258	61	250
	60		713.781									

FINAL

REVIEWER SL6

60 44.281 0.7488 0.778 422.3 1.7088

SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORAHUMOKA, FC JOB NO.: 10382
 SAMPLE LOCATION: Unit 1 SDA Inlet RUN NO.: 1-I-M101A-3
 BAR. PRESS., IN. HG: 29.9 STATIC PRESSURE, IN. H₂O: -2.5 DATE: 3/4/98
 LEAK ✓ VAC., IN. HG: 15 6 10 RUN TIME: 1145 - 1254
 LEAK RATE, CFM: 0.005 0.006 0.002 TEST PERSONS: STB, HDD

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@		XAD	WT.			
PITOT	✓	✓	N30	0.9647	1.83					NA	
TC	✓	✓	PITOT ID	Cp	METER TEMP.						
NOZZLE	✓	✓	PT 12	0.84	80						
ORSAT	✓	NA	TC READOUT	TC	EST. % H ₂ O						
			F107	62	12						
			NOZZLE NO.	DIA.	"C" FACTOR						
			G2007	0.256	0.867						
			SAMPLE BOX	REAGNT.	STACK TEMP.						
			08	217	420						
			UMBILICAL		REF DELTA-P						
			U10		0.790						
			ORSAT PUMP	BAG	"K" FACTOR						
			OR 2	201 B	2.329						

LEAK CHECKS	B	E	B	E	B	E	FYRITES	% O ₂	% CO ₂
	342.978								
	743.030								

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	C-8	0	714.500	0.78	74	421	1.80	1.795	2	258	61	240
2	7	2.5	716.40	0.75	74	421	1.72	1.723	2	250	56	242
3	6	5	718.27	0.77	74	422	1.77	1.767	2	248	54	243
	5	7.5	720.07	0.80	75	422	1.84	1.839	3	248	53	245
	4	10	721.98	0.75	76	423	1.73	1.725	3	255	53	247
6	3	12.5	723.82	0.73	77	420	1.69	1.688	3	260	54	250
7	2	15	725.66	0.68	78	420	1.58	1.576	3	255	56	250
8	1	17.5	727.43	0.63	79	410	1.48	1.480	4	250	57	248
9	B-8	20/0	729.154	0.74	77	415	1.72	1.722	4	230	59	256
10	7	2.5	730.99	0.72	78	415	1.68	1.678	4	240	60	250
11	6	5	732.80	0.64	78	417	1.49	1.488	4	255	61	250
12	5	7.5	734.52	0.60	79	415	1.40	1.402	4	265	56	250
13	4	10	736.19	0.57	79	416	1.33	1.330	5	258	56	245
14	3	12.5	737.82	0.64	80	418	1.50	1.495	5	255	57	247
15	2	15	739.55	0.62	80	415	1.45	1.453	5	250	57	250
16	1	17.5	741.26	0.60	81	414	1.41	1.410	5	250	57	248
17	A-8	40/0	742.978	0.68	80	418	1.59	1.588	5	232	56	250
18	7	2.5	744.81	0.74	81	423	1.72	1.721	6	245	56	250
19	6	5	746.63	0.75	81	425	1.74	1.740	7	248	56	250
20	5	7.5	748.51	0.73	82	424	1.70	1.698	7	258	57	250
21	4	10	750.37	0.70	83	423	1.63	1.633	7	263	57	243
22	3	12.5	752.20	0.75	84	423	1.75	1.754	8	254	58	245
23	2	15	754.05	0.67	84	422	1.57	1.568	8	252	58	250
	1	17.5	755.86	0.63	84	418	1.48	1.482	8	253	58	250
		60	757.625									

FINAL

REVIEWER

SC6

60 43.073 0.6931 79.1 419.2 1.6154

SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, OK JOB NO.: 10382
 SAMPLE LOCATION: Unit 1 SDA Inlet RUN NO.: 1-I-M101A-4
 BAR. PRESS., IN. HG: 29.9 STATIC PRESSURE, IN. H₂O: -3.0 DATE: 3/4/98
 LEAK ✓ VAC., IN. HG: 15 12 RUN TIME: 1354 - 1458
 LEAK RATE, CFM: 0.000 0.000 TEST PERSONS: STB, HDD

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX			DELTA H@			XAD	WT.	
PITOT	✓	✓	<u>N30</u>	Y	<u>0.9647</u>		<u>1.83</u>				
TC	✓	✓	PITOT ID <u>PT 15</u>	Cp	<u>0.84</u>	METER TEMP.	<u>80</u>			<u>NA</u>	
NOZZLE	✓	✓	TC READOUT <u>F107</u>	TC		EST. % H ₂ O	<u>12</u>				
ORSAT	✓	NA	NOZZLE NO. <u>GN 2003</u>	DIA.	<u>0.255</u>	"C" FACTOR	<u>0.867</u>				
			SAMPLE BOX <u>07</u>	REAGNT.	<u>203</u>	STACK TEMP.	<u>420</u>				
			UMBILICAL <u>U10</u>			REF DELTA-P	<u>0.802</u>				
			ORSAT PUMP <u>OR 2</u>	BAG	<u>203 A</u>	"K" FACTOR	<u>2.295</u>				

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

	PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	A-8	0	758.000	0.75	71	420	1.70	1.693	2	248	55	240
2	7	2.5	759.92	0.72	71	418	1.63	1.627	2	250	55	243
3	6	5	761.73	0.70	72	418	1.59	1.585	2	255	55	245
	5	7.5	763.48	0.63	73	414	1.44	1.436	2	260	56	247
	4	10	765.17	0.73	74	415	1.67	1.665	3	260	56	250
6	3	12.5	766.98	0.73	76	414	1.67	1.672	3	262	57	250
7	2	15	768.81	0.76	77	412	1.75	1.748	4	265	57	247
8	1	17.5	770.67	0.70	78	417	1.60	1.604	4	265	58	250
9	B-8	20/0	772.482	0.83	78	416	1.91	1.905	5	255	58	240
10	7	2.5	774.47	0.80	80	419	1.84	1.835	5	254	55	242
11	6	5	776.40	0.85	81	426	1.94	1.938	5	252	55	244
12	5	7.5	778.40	0.76	82	428	1.73	1.732	5	253	56	247
13	4	10	780.25	0.68	83	424	1.56	1.560	5	253	56	250
14	3	12.5	782.12	0.74	84	426	1.70	1.698	6	251	57	250
15	2	15	783.87	0.72	84	426	1.65	1.649	6	252	57	250
16	1	17.5	785.71	0.60	85	421	1.39	1.385	6	252	57	248
17	C-8	40/0	787.401	0.88	84	424	2.02	2.022	8	252	58	246
18	7	2.5	789.48	0.92	85	429	2.10	2.103	8	250	58	248
19	6	5	791.60	0.88	86	426	2.02	2.021	9	250	58	250
20	5	7.5	793.63	0.77	87	427	1.77	1.770	9	250	59	249
21	4	10	795.57	0.75	88	426	1.73	1.730	9	253	59	250
22	3	12.5	797.46	0.70	88	425	1.66	1.663	9	253	59	250
23	2	15	799.32	0.72	88	424	1.67	1.665	9	253	60	250
	1	17.5	801.17	0.64	88	425	1.48	1.479	9	251	60	250
		60	802.930									

1416

1438

FINAL 60 44.930 0.7470 81.0 421.7 1.7175 REVIEWER SLG

SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, FC JOB NO.: 10387
 SAMPLE LOCATION: Unit 1 SDA Inlet RUN NO.: 1-E-M101A-5
 BAR. PRESS., IN. HG: 29.9 STATIC PRESSURE, IN. H₂O: -2.70 DATE: 3/4/98
 LEAK ✓ VAC., IN. HG: 15 10 RUN TIME: 1523-1628
 LEAK RATE, CFM: 0.006 0.00 TEST PERSONS: STB, HDD

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@				XAD	WT.	
PITOT	✓	✓	<u>N20</u>	<u>0.9647</u>		<u>1.83</u>				<u>NA</u>	
TC	✓	✓	PITOT ID <u>6-16</u>	Cp <u>0.84</u>	METER TEMP. <u>80</u>						
NOZZLE	✓	✓	TC READOUT <u>F107</u>	TC <u>25</u>	EST. % H ₂ O <u>12</u>						
ORSAT	✓	NA	NOZZLE NO. <u>2007</u>	DIA. <u>0.256</u>	"C" FACTOR <u>0.866</u>						
			SAMPLE BOX <u>08</u>	REAGNT. <u>203</u>	STACK TEMP. <u>420</u>						
			UMBILICAL <u>110</u>		REF DELTA-P <u>0.790</u>						
			ORSAT PUMP <u>DR 2</u>	BAG <u>148A</u>	"K" FACTOR <u>2.329</u>						

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

	PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	C-8	0	803.200	0.90	78	420	2.09	2.089	2	232	49	240
2	7	2.5	805.35	0.85	78	424	1.96	1.959	2	232	49	239
3	6	5	807.39	0.81	79	427	1.86	1.864	2	250	49	242
4	5	7.5	809.32	0.68	79	421	1.58	1.576	2	250	50	245
5	4	10	811.12	0.65	80	420	1.51	1.512	3	250	50	247
6	3	12.5	812.87	0.67	81	417	1.57	1.567	3	252	50	250
7	2	15	814.65	0.65	82	418	1.52	1.521	3	253	51	249
8	1	17.5	816.42	0.65	82	420	1.52	1.518	3	254	51	250
9	B-8	20/0	818.172	0.80	81	425	1.85	1.854	4	251	52	250
10	7	25	820.100	0.82	82	427	1.90	1.898	5	255	53	250
11	6	50	822.06	0.73	82	427	1.69	1.690	5	260	53	250
12	5	75	823.93	0.62	83	421	1.45	1.448	5	262	55	247
13	4	10	825.62	0.58	84	420	1.36	1.357	5	262	55	249
14	3	12.5	827.31	0.65	84	422	1.52	1.521	5	260	56	250
15	2	15	829.06	0.65	85	421	1.52	1.524	5	258	57	250
16	1	17.5	830.78	0.57	85	418	1.34	1.341	5	256	57	250
17	A-8	40/0	832.448	0.64	84	415	1.51	1.510	6	255	58	249
18	7	25	834.24	0.67	84	417	1.58	1.577	6	256	58	249
19	6	5	836.03	0.65	84	415	1.53	1.533	6	256	59	250
20	5	7.5	837.80	0.70	84	414	1.65	1.653	7	255	59	250
21	4	10	839.67	0.75	85	414	1.77	1.774	7	254	60	250
22	3	12.5	841.57	0.70	85	414	1.66	1.655	7	253	60	248
23	2	15	843.43	0.63	86	414	1.49	1.493	7	252	61	249
	1	17.5	845.20	0.58	86	413	1.38	1.376	7	252	61	247
		60	846.927									

FINAL

REVIEWER SC6

60 43.727 0.6891 82.6 419.4 1.6174

BEST AVAILABLE COPY

SAMPLING DATA - METHOD (S) EPA 101A MOD.

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, OK JOB NO.: 10382
 PLE LOCATION: Unit 1 SDA Inlet RUN NO.: 1-EM101A-6
 BAR PRESS., IN. HG: 29.9 STATIC PRESSURE, IN. H₂O: -2.6 DATE: 3/14/98
 LEAK VAC., IN. HG: 15 11 RUN TIME: 1658 - 1803
 LEAK RATE, CFM: 0.007 0.003 TEST PERSONS: STB, HDID

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H ₂ O	XAD	WT.				
PITOT	✓	✓	<u>N 30</u>	<u>0.9647</u>	<u>1.83</u>						
TC	✓	✓	PITOT ID <u>PT 15</u>	<u>0.84</u>	METER TEMP. <u>80</u>					<u>NA</u>	
NOZZLE	✓	✓	TC READOUT <u>F107</u>	TC	EST. % H ₂ O <u>12</u>						
ORSAT	✓	NA	NOZZLE NO. <u>GN2003</u>	DIA. <u>0.255</u>	"C" FACTOR <u>0.867</u>						
			SAMPLE BOX <u>08</u>	REAGNT. <u>216/218</u>	STACK TEMP. <u>420</u>						
			UMBILICAL <u>U10</u>		REF DELTA-P <u>0.802</u>						
			ORSAT PUMP <u>DR 2</u>	BAG <u>201</u>	"K" FACTOR <u>2.294</u>						

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

	PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP. °F	STACK TEMP. °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER BOX	IMPINGER EXT	PROBE OR COND. EXT
1	A-8	0	847.200	0.67	74	418	1.52	1.524	2	270	57	238
2	7	2.5	849.01	0.71	74	420	1.61	1.609	2	260	57	241
3	6	5	850.80	0.70	75	421	1.59	1.587	2	240	58	243
	5	7.5	852.60	0.74	76	420	1.68	1.683	3	245	58	245
	4	10	854.41	0.68	78	420	1.55	1.552	3	247	58	246
6	3	12.5	856.15	0.76	79	419	1.74	1.741	4	251	58	250
7	2	15	858.03	0.70	80	419	1.61	1.605	4	250	58	250
8	1	17.5	859.82	0.64	81	417	1.47	1.474	4	255	59	248
9	B-8	20/0	861.544	0.73	81	418	1.68	1.680	5	252	59	250
10	7	2.5	863.38	0.78	82	421	1.79	1.792	5	255	59	250
11	6	5	865.29	0.71	83	422	1.63	1.632	5	254	59	250
12	5	7.5	867.10	0.67	84	424	1.54	1.540	5	257	53	248
13	4	10	868.86	0.61	85	422	1.41	1.408	5	259	53	247
14	3	12.5	870.56	0.65	86	422	1.50	1.503	6	261	53	248
15	2	15	872.34	0.63	87	422	1.46	1.459	6	262	53	249
16	1	17.5	874.03	0.58	87	421	1.35	1.346	6	265	54	250
17	C-8	40/0	875.698	0.82	87	420	1.91	1.905	7	264	52	250
18	7	2.5	877.66	0.77	88	423	1.78	1.784	8	262	53	247
19	6	5	879.60	0.72	89	420	1.68	1.677	8	260	53	248
20	5	7.5	881.45	0.80	90	430	1.85	1.846	8	258	53	250
21	4	10	883.44	0.77	91	426	1.79	1.788	9	258	54	250
22	3	12.5	885.38	0.75	92	425	1.75	1.747	9	260	54	250
23	2	15	887.28	0.73	93	425	1.70	1.703	9	260	54	251
	1	17.5	889.16	0.65	93	427	1.51	1.513	9	259	54	250
		60	890.933									

1720

1743

FINAL

REVIEWER SLG

60 43,733 0.7058 84.0 421.8 1.6292

APPENDIX C

FIELD DATA

1.0 UNIT NO. 1

b. STACK

METHOD 3 (ORSAT) FIELD DATA

BEST AVAILABLE COPY

Client OGDEN ENERGY GROUP
 Plant Name OMS LAKE
 City/State OKLAHOMA, FL
 Sampling Location UNIT NO. 1 OUTLET

Job No. 10382
 Fuel Type MUNI WASTE

Run/Sample No. <u>1-0-m3-1</u> Date <u>3/4/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
0835	1029	7.4	19.6	—	12.2	—	
1	1037	7.2	19.5	—	12.3	—	
0935	1044	7.2	19.5	—	12.3	—	
Avg.		7.3	Avg.		12.3	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. _____		F _o _____			

Run/Sample No. <u>1-0-m3-2</u> Date <u>3/4/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1010	1140	8.0	19.6	—	11.6	—	
1	1147	8.0	19.6	—	11.6	—	
1113	1154	8.0	19.6	—	11.6	—	
Avg.		8.0	Avg.		11.6	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B200</u>		F _o _____			

Run/Sample No. <u>1-0-m3-3</u> Date <u>3/4/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1145	1330	8.0	19.6	—	11.6	—	
1	1340	8.0	19.5	—	11.5	—	
1249	1348	8.0	19.6	—	11.6	—	
Avg.		8.0	Avg.		11.6	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B148</u>		F _o _____			

METHOD 3 (ORSAT) FIELD DATA

Client OGDEN ENERGY GROUP

Job No. 10382

Plant Name OMS LAKE

Fuel Type MUNI WASTE

City/State OKLAHOMA, FL

Sampling Location UNIT No. 1 OUTLET

Run/Sample No. <u>1-0-M3-4</u> Date <u>3/4/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1354	1612	7.9	19.5	—	11.6	—	
1	1620	7.9	19.5	—	11.6	—	
1457	1630	7.9	19.5	—	11.6	—	
Avg.		7.9	Avg.		11.6	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B200</u>		F _o _____			

Run/Sample No. <u>1-0-M3-5</u> Date <u>3/4/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1522	1736	7.7	19.5	—	11.8 [⊙]	—	
1	1743	7.8	19.5	—	11.7 [⊙]	—	
1626	1750	7.8	19.5	—	11.7	—	
Avg.		7.8	Avg.		11.7	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B202</u>		F _o _____			

Run/Sample No. <u>1-0-M3-6</u> Date <u>3/4/98</u> Leak <input type="checkbox"/> OK? <input type="checkbox"/>							Operator <u>gtp</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1658	1840	7.6	19.8	—	12.2	—	
1	1850	7.5	19.8	—	12.3	—	
1801	1856	7.6	19.8	—	12.2	—	
Avg.		7.6	Avg.		12.2	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B203</u>		F _o _____			

ABORT

SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: DODEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORAHUMPKA, FC JOB NO.: 10382
 SAMPLE LOCATION: Unit 1 FF Outlet RUN NO.: 1-0-M101A-1
 BAR. PRESS., IN. HG: 29.9 STATIC PRESSURE, IN. H₂O: -18.1 DATE: 3/4/98
 LEAK ✓ VAC., IN. HG: 15 11 RUN TIME: 0835 - 0939
 LEAK RATE, CFM: 0.002 0.000 TEST PERSONS: WAT

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y		DELTA H@			XAD	WT.	
PITOT	✓	✓	<u>N-22</u>		<u>0.9988</u>	<u>1.834</u>			<u>NA</u>	<u>NA</u>	
TC	✓	✓	PITOT ID	Cp	<u>0.84</u>	METER TEMP.	<u>70</u>				
NOZZLE	✓	✓	TC READOUT	TC	<u>24</u>	EST. % H ₂ O	<u>17</u>				
ORSAT	✓	NA	NOZZLE NO.	DIA.	<u>0.217</u>	"C" FACTOR	<u>0.755</u>				
			SAMPLE BOX	REAGNT.	<u>211</u>	STACK TEMP.	<u>280</u>				
			UMBILICAL		<u>U95</u>	REF DELTA-P	<u>1.477</u>				
			ORSAT PUMP	BAG	<u>0R1</u>	"K" FACTOR	<u>1.245</u>				

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			<u>7% Bay</u>

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-8	0	693.55	1.21	56	276	1.49	1.42	3	248	56	
2	7	25	645.325	1.25	57	282	1.49	1.493	3	257	58	
3	6	50	646.550	1.27	58	282	1.52	1.520	3	259	59	
4	5	75	648.625	1.30	60	282	1.56	1.562	3	257	60	
5	4	100	650.305	1.20	61	281	1.45	1.446	3	260	60	
6	3	125	651.935	1.00	63	280	1.200	1.212	3	252	62	
7	2	150	653.430	0.97	64	279	1.18	1.186	3	253	63	
8	1	175	654.933	0.75	65	269	0.93	0.927	2	258	62	
9	B-8	200	656.35	1.02	65	272	1.25	1.25	2	260	63	
10	7	225	657.950	0.98	66	282	1.19	1.192	2	258	63	
11	6	250	659.44	0.85	67	284	1.03	1.033	2	261	64	
12	5	275	660.848	0.90	68	283	1.10	1.098	2	246	63	
13	4	300	662.286	0.97	69	282	1.19	1.188	2	235	64	
14	3	325	663.775	0.94	69	280	1.15	1.154	2	253	64	
15	2	350	665.248	0.95	70	281	1.17	1.167	2	244	62	
16	1	375	666.732	0.80	71	274	1.00	0.994	2	250	61	
17	C-8	40.0	668.21	1.06	70	275	1.35	1.313	2	246	61	
18	7	425	669.800	1.10	71	287	1.34	1.342	2	256	62	
19	6	450	671.375	1.13	71	288	1.38	1.377	2	258	62	
20	5	475	672.977	1.09	72	288	1.33	1.331	2	254	61	
21	4	500	674.55	1.08	72	286	1.32	1.322	2	256	62	
22	3	525	676.137	1.00	73	286	1.23	1.227	2	250	62	
23	2	550	677.632	0.82	73	282	1.00	1.011	2	245	63	
24	1	575	679.035	0.95	73	267	1.20	1.197	2	264	64	
25	END	600	680.510									

FINAL

REVIEWER SCG

60 36.96 1.0204 668 280.5 1.250

13

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SAMPLING DATA - METHOD (S) EPA 101A

Page 1 of 1

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, OK JOB NO.: 10387
 SAMPLE LOCATION: Unit 1 FF Outlet RUN NO.: 1-0-M101A-2
 BAR. PRESS., IN. HG: 29.9 STATIC PRESSURE, IN. H₂O: ~~29.7~~ 176 DATE: 3/4/98
 LEAK ✓ VAC., IN. HG: 11 6 ⊖ RUN TIME: 1010 - 1113
 LEAK RATE, CFM: 0.004 0.000 TEST PERSONS: WAT

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH		FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@		XAD	WT.		
PITOT	✓	✓	<u>PT-14</u>	Cp <u>084</u>	METER TEMP.	<u>70</u>	NA	NA		
TC	✓	✓	TC READOUT <u>Fuji</u>	TC <u>49</u>	EST. % H ₂ O	<u>17</u>				
NOZZLE	✓	✓	NOZZLE NO. <u>GM292</u>	DIA. <u>0.217</u>	"C" FACTOR	<u>0.755</u>				
ORSAT	✓	NA	SAMPLE BOX <u>64</u>	REAGNT. <u>202</u>	STACK TEMP.	<u>280</u>				
			UMBILICAL <u>W95</u>		REF DELTA-P	<u>141.457</u>				
			ORSAT PUMP <u>021</u>	BAG <u>B200</u>	"K" FACTOR	<u>129.205</u>				

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			
							<u>87.8%</u>

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-8	0	686.7	1.19	67	279	1.46	1.458	2	255	64	
2	7	25	682.490	1.15	67	287	1.39	1.393	2	245	61	
3	6	50	684.080	1.15	67	285	1.40	1.397	2	256	60	
	5	75	685.705	1.0	68	284	1.22	1.218	2	280	60	
	4	100	687.190	1.03	69	283	1.26	1.268	2	255	61	
6	3	125	688.717	0.89	70	283	1.09	1.09	2	245	61	
7	2	150	690.170	0.85	70	284	1.04	1.040	2	255	60	
8	1	175	691.572	0.65	71	268	0.82	0.85	2	245	60	
9	B-8	200	692.910	0.97	71	283	1.20	1.199	2	243	61	
10	7	225	694.456	0.98	71	289	1.20	1.200	2	248	62	
11	6	250	695.960	0.95	72	289	1.17	1.166	2	246	62	
12	5	275	697.460	0.97	72	287	1.19	1.188	2	253	61	
13	4	300	698.935	1.05	73	285	1.29	1.292	2	249	62	
14	3	325	700.510	1.11	75	284	1.38	1.327	2	253	62	
15	2	350	702.120	1.13	76	285	1.40	1.397	2	247	63	
16	1	375	703.75	0.75	78	269	0.95	0.951	2	259	63	
17	C-8	400	705.22	1.10	77	280	1.37	1.373	2	247	62	
18	7	425	706.885	1.09	78	286	1.35	1.351	2	255	63	
19	6	450	708.480	0.95	79	287	1.18	1.178	2	245	63	
20	5	475	709.967	0.94	80	286	1.17	1.170	2	251	63	
21	4	500	711.452	0.90	80	285	1.12	1.122	2	246	63	
22	3	525	712.915	0.93	80	285	1.16	1.159	2	247	63	
23	2	550	714.380	0.88	80	285	1.10	1.097	2	254	61	
	1	575	715.820	0.60	80	272	0.76					
	B-0	600	717.055									
FINAL												

60 36:355 0.9609 73.8 282.9 1.1946

REVIEWER SC6

SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORLANDO, FL JOB NO.: 10382
 SAMPLE LOCATION: Unit 1 FF Outlet RUN NO.: 1-0-M101A-3
 BAR PRESS., IN. HG: 29.9 STATIC PRESSURE, IN. H₂O: -17.6 DATE: 3/4/98
 LEAK ✓ VAC., IN. HG: 12 5 RUN TIME: 1145 - 1249
 LEAK RATE, CFM: 0.002 0.000 TEST PERSONS: WJ

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX		Y	DELTA H ₂ O			XAD	WT.	
PITOT	✓	✓	PITOT ID	<u>PT7</u>	Cp	<u>0.94</u>	METER TEMP.	<u>80</u>	N/A	N/A	
TC	✓	✓	TC READOUT	<u>Fuji</u>	TC	<u>24</u>	EST. % H ₂ O	<u>17</u>			
NOZZLE	✓	✓	NOZZLE NO.	<u>60286</u>	DIA.	<u>0.217</u>	"C" FACTOR	<u>0.761</u>			
ORSAT	✓	NA	SAMPLE BOX	<u>73</u>	REAGNT.	<u>211</u>	STACK TEMP.	<u>280</u>			
			UMBILICAL	<u>U95</u>			REF DELTA-P	<u>1.469</u>			
			ORSAT PUMP	<u>021</u>	BAG	<u>B148</u>	"K" FACTOR	<u>1.251</u>			

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			<u>82.8%</u>

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-8	0	717.200	1.18	75	282	1.47	1.466	3	241	60	
2	7	25	719.096	1.16	75	288	1.43	1.428	3	259	56	
3	6	50	720.735	1.15	75	285	1.42	1.416	3	242	56	
4	5	75	722.228	1.17	76	287	1.45	1.445	3	253	55	
5	4	100	724.025	0.95	76	288	1.17	1.172	2	250	57	
6	3	125	725.556	0.98	77	287	1.21	1.213	3	244	58	
7	2	150	727.065	0.88	78	282	1.10	1.099	3	250	58	
8	1	175	728.530	0.66	79	267	0.84	0.843	3	254	57	
9	B-8	200	729.865	0.88	78	279	1.10	1.104	3	252	58	
10	7	225	731.25	0.86	80	284	1.08	1.075	3	242	58	
11	6	250	732.76	0.86	81	285	1.08	1.076	3	254	58	
12	5	275	734.190	0.88	81	286	1.10	1.099	3	241	59	
13	4	300	735.645	0.92	82	285	1.15	1.153	3	257	59	
14	3	325	737.15	0.95	83	288	1.19	1.188	3	253	60	
15	2	350	738.640	0.97	83	287	1.21	1.214	3	242	60	
16	1	375	740.180	0.77	84	268	1.00	0.991	3	245	61	
17	C-8	400	741.62	1.13	84	285	1.42	1.422	3	244	63	
18	7	425	743.285	1.04	85	291	1.3	1.299	2	255	63	
19	6	450	744.885	0.99	86	291	1.24	1.237	2	245	62	
20	5	475	746.427	1.05	87	291	1.32	1.315	2	255	63	
21	4	500	748.085	1.05	88	290	1.32	1.319	2	253	64	
22	3	525	749.565	1.04	88	290	1.31	1.306	2	243	64	
23	2	550	751.150	0.90	87	288	1.13	1.131	2	249	63	
24	1	575	752.635	0.86	87	269	1.03	1.032	2	249	63	
25	END	600	754.03									

FINAL

REVIEWER SLG

60 36.73 0.9628 815 284.4 1.2113 1.2133 (SF)

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SAMPLING DATA - METHOD (S) EPA 101A

Page 1 of 1

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, OK JOB NO.: 10382
 SAMPLE LOCATION: Unit 1 FF Outlet RUN NO.: 1-0-M101A-4
 BAR PRESS., IN. HG: 29.9 STATIC PRESSURE, IN. H₂O: -18.3 DATE: 3/4/98
 LEAK ✓ VAC., IN. HG: 16 5 RUN TIME: 1354-1457
 LEAK RATE, CFM: 0.000 0.000 TEST PERSONS: WJW

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX		Y	DELTA H@			XAD	WT.	
PITOT	✓	✓	PITOT ID	<u>PT-14</u>	Cp	<u>0.84</u>	METER TEMP.	<u>85</u>	NA	NA	
TC	✓	✓	TC READOUT	<u>Fuji</u>	TC	<u>49</u>	EST. % H ₂ O	<u>17</u>			
NOZZLE	✓	✓	NOZZLE NO.	<u>GN292</u>	DIA.	<u>0.217</u>	"C" FACTOR	<u>0.768</u>			
ORSAT	✓	NA	SAMPLE BOX	<u>64</u>	REAGNT.	<u>202</u>	STACK TEMP.	<u>280</u>			
			UMBILICAL	<u>U95</u>			REF DELTA-P	<u>1.452</u>			
			ORSAT PUMP	<u>OR1</u>	BAG	<u>B200</u>	"K" FACTOR	<u>1.267</u>			

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			
							<u>8% O₂ 8% CO₂</u>

	PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	A-8	0	754.250	1.08	69	283	1.33	1.325	2	250	53	
2	7	25	755.958	0.98	69	284	1.20	1.200	2	253	53	
3	6	5:0	757.47	0.95	69	285	1.16	1.162	2	249	49	
	5	7:5	758.94	0.91	70	285	1.12	1.115	2	239	49	
	4	10:0	760.395	0.93	70	286	1.14	1.138	2	261	50	
6	3	12:5	761.865	0.80	71	282	0.99	0.986	2	263	53	
7	2	15:0	763.255	0.79	73	283	0.98	0.976	2	251	54	
8	1	17:5	764.625	0.60	74	267	0.76	0.759	2	255	54	
9	B-8	20:0	765.86	0.94	74	282	1.17	1.166	2	259	55	
10	7	22:5	767.380	0.93	75	286	1.15	1.149	2	249	54	
11	6	25:0	768.982	0.94	77	284	1.17	1.168	2	249	54	
12	5	27:5	770.372	0.89	78	287	1.10	1.100	2	256	55	
13	4	30:0	771.830	0.96	78	286	1.19	1.189	2	247	56	
14	3	32:5	773.325	1.05	80	287	1.30	1.308	2	250	57	
15	2	35:0	774.910	0.83	80	285	1.03	1.032	2	257	59	
16	1	37:5	776.302	0.64	81	269	0.82	0.815	2	242	60	
17	C-8	40:0	777.600	1.05	81	283	1.31	1.313	2	248	63	
18	7	42:5	779.242	1.05	82	287	1.31	1.307	2	257	60	
19	6	45:0	780.812	1.05	83	289	1.31	1.306	2	250	60	
20	5	47:5	782.400	1.06	84	291	1.32	1.317	2	253	59	
21	4	50:0	783.995	1.00	85	291	1.245	1.245	2	250	60	
22	3	52:5	785.580	0.96	85	286	1.2	1.204	2	251	60	
23	2	55:0	787.055	0.94	85	284	1.18	1.182	2	253	61	
	1	57:5	788.55	0.73	85	272	0.93	0.933	2	256	61	
	END	60:0	789.938									

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REVIEWER SLV

35.708 0.9144 77.4 288.5 1.1423

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SAMPLING DATA - METHOD (S) EPA 101A

Page 1 of 1

CLIENT: DODEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, FC JOB NO.: 10382
 SAMPLE LOCATION: UNIT 1 FF Outlet RUN NO.: 1-0-M101A-5
 BAR. PRESS., IN. HG: 29.9 STATIC PRESSURE, IN. H₂O: -16.5 DATE: 3/4/98
 LEAK ✓ VAC., IN. HG: 10 5 RUN TIME: 1522 - 1626
 LEAK RATE, CFM: 0.002 0.000 TEST PERSONS: WAT

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER		TARE	
	PRE	POST	METER BOX	N-22	Y	0.9488	DELTA H@	1.834		XAD	WT.		
PITOT	✓	✓	PITOT ID	PT-7	Cp	0.04	METER TEMP.	80		NA	NA		
TC	✓	✓	TC READOUT	Fuji	TC	24	EST. % H ₂ O	17					
NOZZLE	✓	✓	NOZZLE NO.	GN286	DIA.	0.217	"C" FACTOR	0.759					
ORSAT	✓	NA	SAMPLE BOX	73	REAGNT.	RB211	STACK TEMP.	280					
			UMBILICAL	U95			REF DELTA-P	1.470					
			ORSAT PUMP	OR-1	BAG	B202	"K" FACTOR	1.252					

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E		7.5% B _{AP}	

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-2	0	790.100	1.30	78	283	1.62	1.618	2	251	61	
2	7	25	791.925	1.20	78	284	1.49	1.489	2	238	59	
3	6	50	793.618	1.12	78	290	1.38	1.379	2	260	58	
4	5	75	795.242	1.00	78	288	1.24	1.235	2	242	57	
5	4	100	796.77	0.98	79	287	1.21	1.214	2	266	57	
6	3	125	798.285	0.87	80	285	1.08	1.083	2	246	59	
7	2	150	799.735	0.85	80	286	1.06	1.057	2	262	60	
8	1	175	801.170	0.72	81	269	0.92	0.918	2	248	61	
9	B-8	200	802.535	1.00	80	282	1.25	1.251	2	256	59	
10	7	225	804.12	0.97	81	286	1.21	1.208	2	256	60	
11	6	250	805.645	0.90	82	289	1.19	1.119	2	256	60	
12	5	275	807.125	0.90	83	288	1.12	1.122	2	253	63	
13	4	300	808.595	0.95	83	290	1.18	1.182	2	257	62	
14	3	325	810.110	0.98	84	289	1.22	1.223	2	245	63	
15	2	350	811.650	0.94	84	286	1.18	1.177	2	249	63	
16	1	375	813.165	0.75	84	274	0.96	0.955	2	255	62	
17	C-8	400	814.56	1.02	82	283	1.28	1.279	2	258	61	
18	7	425	816.197	0.94	83	287	1.17	1.173	2	251	59	
19	6	450	817.700	0.93	83	286	1.16	1.163	2	253	59	
20	5	475	819.195	0.96	83	287	1.2	1.199	2	253	59	
21	4	500	820.727	0.95	83	287	1.19	1.186	2	254	59	
22	3	525	822.240	0.95	83	286	1.19	1.188	2	255	58	
23	2	550	823.745	0.85	83	287	1.06	1.061	2	239	58	
24	1	575	825.185	0.80	83	279	1.01	1.010	2	260	59	
BNO	600		826.630									

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60 26.53 0.9473 815 2849 1.1875

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SAMPLING DATA - METHOD (S) Mod 101A

Page 1 of 1

CLIENT: DODEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORLANDO, FL JOB NO.: 10382
 SAMPLE LOCATION: Unit 1 FF Outlet RUN NO.: 1-0-MM101A-1
 BAR. PRESS., IN. HG: 29.9 STATIC PRESSURE, IN. H₂O: -18.5 DATE: 3/4/98
 LEAK ✓ VAC., IN. HG: 10 6 RUN TIME: 1658 - 1801
 LEAK RATE, CFM: 0.000 0.000 TEST PERSONS: WAS / HOD

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX		Y	DELTA H@			XAD	WT.	
PITOT	✓	✓	<u>N22</u>		<u>0.9988</u>	<u>1.834</u>			<u>NA</u>	<u>NA</u>	
TC	✓	✓	PITOT ID <u>PP139</u>	Cp	<u>0.84</u>	METER TEMP. <u>80</u>					
NOZZLE	✓	✓	TC READOUT <u>Fuji</u>	TC	<u>12</u>	EST. % H ₂ O <u>17</u>					
ORSAT	✓	NA	NOZZLE NO. <u>GN292</u>	DIA.	<u>0.217</u>	"C" FACTOR <u>0.761</u>					
			SAMPLE BOX <u>30</u>	REAGNT.	<u>Cl4/209</u>	STACK TEMP. <u>280</u>					
			UMBILICAL <u>UG5</u>			REF DELTA-P <u>1.466</u>					
			ORSAT PUMP <u>OR1</u>	BAG	<u>8203</u>	"K" FACTOR <u>1.255</u>					

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			
						<u>8% Bar</u>	<u>8% Bag</u>

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-8	0	826.750	1.10	78	282	1.37	1.371	3	238	58	
2	7	25	828.525	1.03	79	283	1.29	1.286	3	254	56	
3	6	50	830.097	1.00	80	285	1.25	1.248	3	245	56	
	5	75	831.635	0.98	81	284	1.23	1.217	3	247	56	
	4	100	833.140	0.92	82	285	1.15	1.152	3	248	57	
6	3	125	834.623	0.90	83	285	1.13	1.130	3	252	58	
7	2	150	836.108	0.86	85	287	1.08	1.080	3	241	59	
8	1	175	837.560	0.70	85	269	0.90	0.901	3	246	60	
9	B-8	200	838.940	0.88	85	282	1.11	1.114	3	255	61	
10	7	225	840.492	0.85	86	286	1.07	1.071	3	255	61	
11	6	250	841.932	0.84	87	290	1.06	1.055	3	245	62	
12	5	275	843.346	0.86	88	290	1.08	1.082	3	257	62	
13	4	300	844.786	0.93	89	290	1.17	1.172	3	246	62	
14	3	325	846.270	0.99	89	290	1.25	1.248	3	255	63	
15	2	350	847.827	0.96	89	289	1.20	1.211	3	253	63	
16	1	375	849.370	0.75	90	269	0.97	0.974	3	247	64	
17	C-8	400	850.725	0.98	89	274	1.26	1.263	3	243	60	
18	7	425	852.326	1.0	89	290	1.26	1.26	3	244	57	
19	6	450	853.97	0.95	89	291	1.20	1.196	3	255	58	
20	5	475	855.443	1.13	89	289	1.43	1.426	3	237	58	
21	4	500	857.1005	1.04	89	289	1.30	1.312	3	252	59	
22	3	525	858.77	1.05	89	290	1.32	1.32	3	258	59	
23	2	550	860.31	0.75	89	284	0.95	0.953	3	253	60	
	1	575	861.82	0.74	89	267	0.96	0.96	3	247	62	
	ENO	600	863.226									

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REVIEWER SCB

60 36.476 0.92 86 284 1.17

APPENDIX C

FIELD DATA

2.0 UNIT NO. 2

a. INLET

METHOD 3 (ORSAT) FIELD DATA

Client OGDEN ENERGY GROUP
 Plant Name OMS LAKE
 City/State OKLAHOMA, FL
 Sampling Location UNIT No. 2 INLET

Job No. 10382
 Fuel Type MUNI WASTE

Run/Sample No. <u>2-I-M3-1</u> Date <u>3/3/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator
							<u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
0922	1105	8.5	20.6	—	12.1	—	
1	1115	8.5	20.6	—	12.1	—	
1036	1123	8.5	20.6	—	12.1	—	
Avg.		8.5	Avg.		12.1	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B139</u>		F _o <u>1.035</u>			

Run/Sample No. <u>2-I-m3-2</u> Date <u>3/3/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator
							<u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1205	1325	8.7	19.6	—	10.9	—	
1	1335	8.7	19.6	—	10.9	—	
1311	1343	8.7	19.6	—	10.9	—	
Avg.		8.7	Avg.		10.9	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B207</u>		F _o _____			

Run/Sample No. <u>2-I-m3-3</u> Date <u>3/3/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator
							<u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1344	1548	8.8	19.9	—	11.1	—	
1	1600	9.0	19.9	—	10.9	—	
1452	1608	9.0	19.9	—	10.9	—	
Avg.		8.9	Avg.		11.0	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B203</u>		F _o _____			

METHOD 3 (ORSAT) FIELD DATA

Client OGDEN ENERGY GROUP
 Plant Name DMS LAKE
 City/State OKLAHOMA, FL
 Sampling Location UNIT No. 2 INLET

Job No. 10382
 Fuel Type MUNI WASTE

Run/Sample No. <u>2-I-M3-4</u> Date <u>3/3/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1518	1820	9.4	19.6	—	10.2	—	
1	1828	9.4	19.5	—	10.1	—	
1623	1836	9.4	19.6	✓	10.2	—	
Avg.		9.4	Avg.		10.2	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B202</u>		F ₀ _____			

Run/Sample No. <u>2-I-M3-5</u> ^{M3/MMIDA-1} Date <u>3/3/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1655	1843	9.4	19.6	—	10.2	—	
1	1850	9.4	19.5	—	10.1	—	
1803	1857	9.4	19.6	—	10.2	—	
Avg.		9.4	Avg.		10.2	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B201</u>		F ₀ _____			

Run/Sample No. _____ Date _____ Leak <input type="checkbox"/> OK? <input type="checkbox"/>							Operator
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
Avg.			Avg.				
Orsat I.D. _____		Tedlar Bag I.D. _____		F ₀ _____			

SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORAHAMOKA, FC JOB NO.: 10382
 SAMPLE LOCATION: Unit 2 SDA Inlet RUN NO.: 2-I-M101A-1
 BAR. PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: -2.4 DATE: 3/3/98
 LEAK ✓ VAC., IN. HG: 15 10 15 15 RUN TIME: 0920 - 1036
 LEAK RATE, CFM: 0.003 0.005 0.005 0.005 TEST PERSONS: STB, HDD

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX		Y	DELTA H@			XAD	WT.	
PITOT	✓	✓	<u>N30</u>		<u>0.9647</u>	<u>1.83</u>					
TC	✓	✓	PITOT ID <u>PT 12</u>	Cp	<u>0.84</u>	METER TEMP.	<u>75</u>			<u>N/A</u>	
NOZZLE	✓	✓	TC READOUT <u>F107</u>	TC	<u>TC 62</u>	EST. % H ₂ O	<u>12</u>				
ORSAT	✓	NA	NOZZLE NO. <u>GN2004</u>	DIA.	<u>0.255</u>	"C" FACTOR	<u>0.861</u>				
			SAMPLE BOX <u>08</u>	REAGNT.	<u>205</u>	STACK TEMP.	<u>450</u>				
			UMBILICAL <u>U10</u>			REF DELTA-P	<u>0.835</u>				
			ORSAT PUMP <u>OR2</u>	BAG	<u>B139-A</u>	"K" FACTOR	<u>2.203</u>				

LEAK CHECKS	B <u>417.102</u>	B	B	B	FYRITES	% O ₂		
	E <u>417.300</u>	E	E	E		% CO ₂		

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-8	0	389.400	0.77	66	446	1.68	1.676	2	255	55	250
2	7	2.5	391.31	0.71	66	441	1.55	1.551	2	260	51	250
3	6	5	393.1	0.82	67	442	1.77	1.772	3	265	51	255
4	5	7.5	394.81	0.68	68	448	1.48	1.480	3	260	52	250
5	4	10	396.52	0.71	70	456	1.54	1.538	3	262	53	250
6	3	12.5	398.20	0.60	71	461	1.30	1.295	4	263	53	255
7	2	15	399.8	0.62	73	460	1.35	1.346	4	265	54	248
8	1	17.5	401.4	0.65	74	453	1.42	1.42	4	260	55	245
9	B-8	20	403.054	0.86	74	458	1.87	1.870	5	255	58	250
10	7	22.5	405.00	0.90	77	464	1.95	1.953	6	255	56	245
11	6	25	406.98	0.77	78	465	1.88	1.672	6	256	56	240
12	5	27.5	408.83	0.70	79	460	1.53	1.532	6	256	57	245
13	4	30	410.48	0.65	81	457	1.43	1.433	6	259	57	245
14	3	32.5	412.11	0.64	82	455	1.42	1.417	6	259	58	248
15	2	35	413.85	0.63	83	452	1.40	1.402	7	255	58	250
16	1	37.5	415.44	0.63	83	452	1.40	1.402	7	255	59	250
17	C-8	40	417.102	0.91	81	450	2.02	2.023	8	250	57	250
18	7	42.5	419.60	0.87	82	452	1.93	1.926	8	245	58	245
19	6	45	420.96	0.90	83	451	2.0	2.003	9	248	58	245
20	5	47.5	422.88	0.93	84	452	1.63	1.626	10	255	59	248
21	4	50	424.83	0.75	84	455	1.67	1.666	11	258	60	250
22	3	52.5	426.92	0.82	84	457	1.82	1.818	12	260	60	250
23	2	55	428.85	0.77	84	458	1.70	1.704	12	258	61	248
	1	57.5	430.90	0.75	85	457	1.67	1.665	12	260	62	250
		60	432.852									

Res
6946

Est
196

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60 43.452 0.7999 77.5 454.3 1.633

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SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORAHUMPKA, FC JOB NO.: 10382
 SIPLE LOCATION: Unit 2 SDA Inlet RUN NO.: 2-I-M101A-2
 BAR. PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: -2.4 DATE: 3/3/98
 LEAK ✓ VAC., IN. HG: 15 13 RUN TIME: 1205 - 1311
 LEAK RATE, CFM: 0.000 0.000 TEST PERSONS: STB, HDD

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@				XAD	WT.	
PITOT	✓	✓	<u>N 30</u>	<u>0.9647</u>	<u>1.83</u>	<u>1.83</u>					
TC	✓	✓	PITOT ID <u>PT15</u>	<u>084</u>	METER TEMP.	<u>75</u>	<u>78</u>			<u>NA</u>	
NOZZLE	✓	✓	TC READOUT <u>F107</u>	TC	EST. % H ₂ O	<u>12</u>	<u>13.5</u>				
ORSAT	✓	NA	NOZZLE NO. <u>G127</u>	DIA. <u>0.253</u>	"C" FACTOR	<u>0.86</u>	<u>0.836</u>				
			SAMPLE BOX <u>07</u>	REAGNT. <u>205</u>	STACK TEMP.	<u>450</u>	<u>450</u>				
			UMBILICAL <u>U10</u>		REF DELTA-P	<u>0.863</u>	<u>0.888</u>				
			ORSAT PUMP <u>DR2</u>	BAG <u>203-A</u>	"K" FACTOR	<u>2.131</u>	<u>2.072</u>				

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

	PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	A-8	0	433.600	0.86	70	468	1.73	1.732	3	250	57	248
2	7	2.5	435.47	0.87	70	471	1.74	1.743	3	253	55	250
3	6	5	437.33	0.80	71	472	1.60	1.604	3	255	55	250
	5	7.5	439.12	0.77	72	476	1.54	1.541	4	257	55	248
	4	10	440.83	0.81	73	478	1.62	1.621	4	260	56	250
6	3	12.5	442.57	0.78	74	480	1.56	1.560	5	255	56	245
7	2	15	444.32	0.75	76	477	1.51	1.511	5	265	57	248
8	1	17.5	446.05	0.72	77	475	1.46	1.456	5	263	57	245
9	B-8	20/0	447.745	0.96	77	470	1.93	1.932	7	260	58	248
10	7	2.5	449.73	0.95	79	473	1.93	1.931	8	258	58	250
11	6	5	451.72	0.87	80	473	1.77	1.772	7	255	59	250
12	5	7.5	453.63	0.77	81	472	1.57	1.573	7	259	59	248
13	4	10	455.40	0.70	81	473	1.43	1.429	7	259	60	245
14	3	12.5	457.09	0.72	82	474	1.47	1.472	7	255	60	245
15	2	15	458.78	0.67	82	472	1.37	1.372	8	245	61	248
16	1	17.5	460.45	0.62	82	470	1.27	1.273	8	245	62	250
17	C-8	40/0	462.070	0.95	80	470	1.94	1.944	9	240	60	250
18	7	2.5	464.04	0.97	81	468	1.99	1.989	10	240	56	245
19	6	5	466.08	0.93	82	467	1.91	1.913	11	245	56	248
20	5	7.5	468.04	0.77	82	467	1.58	1.584	11	248	56	250
21	4	10	469.80	0.75	82	468	1.54	1.542	11	245	57	250
22	3	12.5	471.60	0.76	83	467	1.57	1.568	11	242	58	245
23	2	15	473.36	0.78	83	468	1.61	1.607	12	245	58	250
	1	17.5	475.15	0.75	84	466	1.55	1.551	12	248	59	245
		60	476.931									

FINAL

REVIEWER SC6

60 43.331 0.806 79.5 471.5 1.6338

SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORAHUMPKA, FL JOB NO.: 10387
 SAMPLE LOCATION: Unit 2 SDA Inlet RUN NO.: 2-T-M101A-3
 BAR. PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: -2.6 DATE: 3/3/98
 LEAK ✓ VAC., IN. HG: 15 12 RUN TIME: 1344-1452
 LEAK RATE, CFM: 0.007 0.003 TEST PERSONS: STB, HDD

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS		NOMOGRAPH		FILTER	TARE
	PRE	POST	METER BOX		DELTA H@		XAD	WT.
PITOT	✓	✓	<u>N30</u>	<u>Y 0.9647</u>	<u>1.83</u>			
TC	✓	✓	PITOT ID <u>PT12</u>	<u>Cp 0.84</u>	METER TEMP. <u>75</u>			<u>NA</u>
NOZZLE	✓	✓	TC READOUT <u>F107</u>	<u>TC 62</u>	EST. % H ₂ O <u>13.5</u>			
ORSAT	✓	NA	NOZZLE NO. <u>GN2003</u>	<u>DIA. 0.255</u>	"C" FACTOR <u>0.836</u>			
			SAMPLE BOX <u>08</u>	REAGNT. <u>205</u>	STACK TEMP. <u>470</u>			
			UMBILICAL <u>U10</u>		REF DELTA-P <u>0.880</u>			
			ORSAT PUMP <u>OR 2</u>	BAG <u>B139-A</u>	"K" FACTOR <u>2.027</u>	<u>2.092</u>		

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

PT. NO.	ELAPSED TIME, MINUTES	DCM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DCM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXT	PROBE OR COND. EXT	
1	A-9	0	477.400	0.73	76	475	1.56	1.526	2	265	58	250
2	7	2.5	479.12	0.75	76	451	1.60	1.604	2	270	57	250
3	6	5	480.87	0.72	76	451	1.54	1.539	2	260	57	245
4	5	7.5	482.61	0.70	77	447	1.51	1.506	3	260	55	248
5	4	10	484.32	0.67	78	450	1.44	1.440	3	258	55	250
6	3	12.5	486.00	0.67	78	456	1.43	1.430	3	258	56	248
7	2	15	487.69	0.65	79	461	1.38	1.383	4	259	56	250
8	1	17.5	489.34	0.65	80	462	1.38	1.384	4	260	57	250
9	B-8	20/0	490.997	0.80	80	458	1.71	1.711	5	256	58	250
10	7	2.5	492.95	0.82	81	455	1.76	1.761	5	257	57	248
11	6	5	494.93	0.80	82	455	1.72	1.721	6	260	58	250
12	5	7.5	496.61	0.68	82	459	1.46	1.457	6	262	58	250
13	4	10	498.31	0.64	83	461	1.37	1.372	6	258	59	245
14	3	12.5	499.96	0.60	83	466	1.28	1.279	6	255	60	245
15	2	15	501.60	0.58	83	463	1.24	1.241	6	252	60	248
16	1	17.5	503.15	0.56	84	461	1.20	1.203	6	250	61	250
17	C-8	20/0	504.725	0.82	83	466	1.75	1.749	7	235	62	245
18	7	2.5	506.61	0.87	83	469	1.85	1.847	8	240	62	248
19	6	5	508.56	0.82	83	460	1.76	1.758	9	245	63	250
20	5	7.5	510.46	0.72	84	457	1.55	1.551	9	252	63	250
21	4	10	512.26	0.68	84	458	1.46	1.464	9	260	63	245
22	3	12.5	513.99	0.75	84	463	1.61	1.607	10	258	64	245
23	2	15	515.82	0.73	85	461	1.57	1.570	10	255	64	248
	1	17.5	517.61	0.73	85	461	1.57	1.570	10	250	64	250
		60	519.400									

1407

1432

FINAL

REVIEWER SLG

60 42.000 0.719 81.2 458.6 1.5292

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SAMPLING DATA - METHOD (S) EPA 101A

Page 1 of 1

CLIENT: DODEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORANMPKA, FC JOB NO.: 10382
 SAMPLE LOCATION: Unit 2 SDA Inlet RUN NO.: 2-I-M101A-4
 BAR. PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: -2.6 DATE: 3/3/98
 LEAK ✓ VAC., IN. HG: 15 12 RUN TIME: 1513 - 1623
 LEAK RATE, CFM: 0.003 0.001 TEST PERSONS: STB, HDD

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS		NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@		XAD	WT.	
PITOT	✓	✓	<u>N 30</u>	<u>0.9647</u>	<u>1.83</u>			<u>NA</u>	
TC	✓	✓	PITOT ID <u>PT15</u>	Cp <u>0.84</u>	METER TEMP. <u>75</u>				
NOZZLE	✓	✓	TC READOUT <u>F107</u>	TC	EST. % H ₂ O <u>13.5</u>				
ORSAT	✓	NA	NOZZLE NO. <u>GN2006</u>	DIA. <u>0.255</u>	"C" FACTOR <u>0.835</u>				
			SAMPLE BOX <u>07</u>	REAGNT. <u>204</u>	STACK TEMP. <u>460</u>				
			UMBILICAL <u>U10</u>	<u>B202-B</u>	REF DELTA-P <u>0.871</u>				
			ORSAT PUMP <u>OR 2</u>	<u>BAC 201-A</u>	"K" FACTOR <u>2.114</u>				

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

	PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	(PROBE OR COND. EXIT)
1	A-8	0	519.700	0.92	80	465	1.95	1.954	2	248	61	240
2	7	2.5	521.74	0.87	80	471	1.83	1.831	2	255	60	243
3	6	5	523.70	0.85	80	473	1.79	1.786	3	265	60	245
	5	7.5	525.58	0.77	81	478	1.61	1.612	3	250	60	248
	4	10	527.38	0.80	82	475	1.68	1.684	3	250	61	250
6	3	12.5	529.23	0.74	83	472	1.57	1.566	4	245	61	250
7	2	15	531.04	0.74	83	475	1.56	1.561	4	252	62	245
8	1	17.5	532.75	0.75	84	474	1.59	1.587	4	248	62	248
9	B-8	20/0	534.557	0.90	83	470	1.910	1.909	5	240	63	245
10	7	2.5	536.54	0.94	83	470	1.99	1.992	5	245	63	248
11	6	5	538.56	0.87	84	471	1.85	1.845	6	250	64	250
12	5	7.5	540.52	0.78	85	473	1.65	1.654	6	255	64	250
13	4	10	542.35	0.66	85	473	1.40	1.400	6	258	62	248
14	3	12.5	544.06	0.68	85	473	1.44	1.443	6	250	62	250
15	2	15	545.76	0.77	85	483	1.62	1.617	7	255	63	250
16	1	17.5	547.60	0.73	85	480	1.54	1.537	7	265	64	248
17	C-8	40/0	549.350	0.92	82	472	1.94	1.943	7	250	62	245
18	7	2.5	551.31	0.95	82	475	2.00	1.998	9	255	63	248
19	6	5	553.34	0.98	81	480	2.05	2.046	10	258	63	250
20	5	7.5	555.40	0.94	81	479	1.97	1.965	10	258	64	250
21	4	10	557.43	0.86	81	481	1.79	1.794	10	260	64	248
22	3	12.5	559.37	0.85	81	483	1.77	1.770	11	258	65	245
23	2	15	561.29	0.85	81	483	1.77	1.770	11	260	65	250
	1	17.5	563.20	0.83	81	482	1.73	1.731	11	260	66	250
		60	565.069									

FINAL 60 45.369 0.8289 82.4 475.5 1.750

REVIEWER SC6

SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORAHAMOKA, FC JOB NO.: 10382
 SAMPLE LOCATION: Unit 2 SDA Inlet RUN NO.: 2-IAM101A-18
 BAR. PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: -2.5 DATE: 3/3/98
 LEAK ✓ VAC., IN. HG: 15 10 RUN TIME: 1655 - 1803
 LEAK RATE, CFM: 0.001 0.001 TEST PERSONS: SAB, HDD

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX		Y	DELTA H@			XAD	WT.	
PITOT	✓	✓	N30		0.9647	1.83					
TC	✓	✓	PPT.16	Cp	0.84	METER TEMP.	75			NA	
NOZZLE	✓	✓	F107	TC	25	EST. % H ₂ O	460	13.5			
ORSAT	✓	NA	GN200T	DIA.	0.256	"C" FACTOR	13.5	0.835			
			09	REAGNT.	618/216	STACK TEMP.	460				
			U10			REF DELTA-P	0.857				
			DR 2	BAG	B201A	"K" FACTOR	2.147				

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

	PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	A-8	0	566.100	0.87	74	473	1.84	1.840	3	242	62	240
2	7	2.5	568.05	0.93	74	475	1.96	1.958	3	260	58	245
3	6	5	570.10	0.80	75	477	1.68	1.684	3	265	58	250
	5	7.5	571.93	0.75	75	474	1.59	1.585	3	260	59	250
	4	10	573.73	0.77	76	474	1.63	1.630	4	260	59	248
6	3	12.5	575.55	0.72	76	475	1.52	1.523	4	258	60	250
7	2	15	577.31	0.70	76	476	1.48	1.479	4	257	60	250
8	1	17.5	579.03	0.67	77	474	1.42	1.422	4	260	61	245
9	B-8	20/0	580.728	0.90	76	472	1.91	1.911	5	248	61	250
10	7	2.5	582.71	0.92	76	471	1.95	1.953	6	252	61	250
11	6	5	584.71	0.70	76	469	1.49	1.489	5	257	60	245
12	5	7.5	586.46	0.65	77	473	1.38	1.381	5	259	60	250
13	4	10	588.14	0.65	77	473	1.38	1.381	5	261	61	250
14	3	12.5	589.81	0.63	77	473	1.34	1.339	6	265	61	248
15	2	15	591.49	0.65	78	471	1.39	1.387	6	260	60	250
16	1	17.5	593.18	0.67	78	473	1.43	1.426	6	260	59	250
17	C-8	40/0	594.872	0.90	77	472	1.91	1.911	7	245	56	240
18	7	2.5	596.85	0.94	77	472	2.00	1.997	8	248	56	243
19	6	5	598.88	0.83	77	474	1.76	1.759	8	253	56	248
20	5	7.5	600.78	0.78	78	474	1.66	1.657	8	257	56	250
21	4	10	602.63	0.74	78	474	1.57	1.573	8	258	57	250
22	3	12.5	604.43	0.77	78	475	1.64	1.635	9	260	57	250
23	2	15	606.27	0.80	78	477	1.70	1.695	9	256	58	248
	1	17.5	608.14	0.76	78	476	1.61	1.612	9	254	58	250
		60	609.952									

(1719)

(1743)

FINAL

REVIEWER

60 43.852 0.7679 76.6 473.6 1.635

APPENDIX C

FIELD DATA

2.0 UNIT NO. 2

b. STACK

METHOD 3 (ORSAT) FIELD DATA

Client OGDEN ENERGY GROUP
 Plant Name OMS LAKE
 City/State OKLAHOMA, FL
 Sampling Location UNIT No. 2 OUTLET

Job No. 10382
 Fuel Type MUNI WASTE

Run/Sample No. <u>2-0-m3-1</u> Date <u>3/3/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
0922	1040	5.8	19.6	—	13.8	—	
1	1048	5.8	19.6	—	13.8	—	
1028	1054	6.0	19.7	—	13.7	—	
Avg.		5.9	Avg.		13.8	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B202</u>		F _o <u>1.203</u>			

Run/Sample No. <u>2-0-m3-2</u> Date <u>3/3/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1205	1359	5.1	19.6	—	14.5	—	
1	1406	5.3	19.7	—	14.4	—	
1319	1416	5.3	19.7	—	14.4	—	
Avg.		5.2	Avg.		14.4	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. _____		F _o _____			

Run/Sample No. <u>2-0-m3-3</u> Date <u>3/3/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1344	1520	8.6	19.5	—	10.9	—	
'	1530	8.4	19.6	—	11.2	—	
1447	1540	8.4	19.6	—	11.2	—	
Avg.		8.5	Avg.		11.1	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B148</u>		F _o _____			

METHOD 3 (ORSAT) FIELD DATA

Client OGDEN ENERGY GROUP
 Plant Name OMS LAKE
 City/State OKLAHOMA, FL
 Sampling Location UNIT NO. 2 OUTLET

Job No. 10382
 Fuel Type MUNI WASTE

Run/Sample No. <u>2-0-M3-4</u> Date <u>3/3/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
	1800	8.7	19.6	—	10.9	—	
	1806	8.7	19.7	—	11.0	—	
	1812	8.7	19.7	—	11.0	—	
Avg.		8.7		Avg.		11.0	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B200</u>		F _o _____			

Run/Sample No. <u>M3/MM1D1A-1</u> 2-0-M3-5 Date <u>3/3/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator <u>SCC</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
	1906	8.0	20.0	—	12.0	—	
	1914	8.5	20.1	—	11.6	—	
	1922	8.5	20.1	—	11.6	—	
Avg.		8.3		Avg.		11.7	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B140</u>		F _o _____			

Run/Sample No. _____ Date _____ Leak <input type="checkbox"/> OK? <input type="checkbox"/>							Operator _____
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
Avg.				Avg.			
Orsat I.D. _____		Tedlar Bag I.D. _____		F _o _____			

SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: DODEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORAHAMPA, FL JOB NO.: 10382
 SAMPLE LOCATION: Unit 2 Outlet FF Duct RUN NO.: 2-0-M101A-1
 BAR. PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: -16.1 DATE: 3/3/98
 LEAK ✓ VAC., IN. HG: 15 6 RUN TIME: 0922 - 1028
 LEAK RATE, CFM: 0.000 0.000 TEST PERSONS: WAT

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	IN 22	Y	0.9988	DELTA H@	1.834		XAD	WT.
PITOT	✓	✓	PITOT ID		Cp	0.84	METER TEMP.	75		NA	NA
TC	✓	✓	TC READOUT	N22	TC	49	EST. % H ₂ O	17			
NOZZLE	✓	✓	NOZZLE NO.	GM295	DIA.	0.217	"C" FACTOR	0.762			
ORSAT	✓	NA	SAMPLE BOX	64	REAGNT.	210	STACK TEMP.	280			
			UMBILICAL	U95			REF DELTA-P	1.464			
			ORSAT PUMP	UR1	BAG	A	"K" FACTOR	1.257			

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E		NA	6%

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-8	0	4154.500	1.35	57	276	1.65	1.651	5	243	56	
2	7	2.5	506.5	1.23	57	282	1.49	1.490	5	241	51	
3	6	5.0	458.158	1.45	58	280	1.77	1.765	5	249	51	
	5	7.5	459.945	1.15	59	281	1.400	1.400	5	238	51	
	4	10.0	461.550	1.15	60	281	1.400	1.404	4	245	52	
6	3	12.5	463.171	0.94	61	280	1.15	1.151	4	245	52	
7	2	15.0	464.640	0.84	62	278	1.03	1.025	4	241	58	
8	1	17.5	466.027	0.59	63	270	0.73	0.738	3	239	59	
9	B-8	20.0	467.180	1.250	62	280	1.52	1.523	4	244	60	
10	17	22.5	469.33	1.157	64	283	1.40	1.402	4	241	60	
11	6	25.0	470.945	1.10	65	284	1.34	1.339	4	249	63	
12	5	27.5	472.575	1.00	66	284	1.22	1.218	4	248	63	
13	4	30.0	474.035	1.04	67	283	1.27	1.273	4	247	64	
14	3	32.5	475.578	1.03	67	283	1.26	1.261	4	238	64	
15	2	35.0	477.126	0.910	68	281	1.12	1.119	4	246	66	
16	1	37.5	478.860	0.60	68	271	0.750	0.758	3	248	60	
17	C-8	40.0	479.750	1.30	68	284	1.59	1.594	4	241	67	
18	7	42.5	481.500	1.40	69	286	1.71	1.712	4	246	66	
19	6	45.0	483.350	1.35	71	286	1.66	1.656	4	246	65	
20	5	47.5	485.115	1.26	71	288	1.54	1.542	4	238	65	
21	4	50.0	486.815	1.23	72	289	1.51	1.506	4	248	66	
22	3	52.5	488.494	1.15	72	292	1.40	1.403	4	244	66	
23	2	55.0	490.13	0.96	72	287	1.18	1.177	4	247	65	
	1	57.5	491.605	0.76	71	268	0.96	0.957	3	242	65	
	END	60.0	492.987									

FINAL

REVIEWER SLC

60 38.497 1.078 654 2816 1.335

BEST AVAILABLE COPY

SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORAHUMPKA, FC JOB NO.: 10382
 SAMPLE LOCATION: Unit 2 FF Outlet Duct RUN NO.: 2-0-M101A-2
 BAR PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: -16.4" DATE: 3/3/98
 LEAK ✓ VAC., IN. HG: 15 6 RUN TIME: 1205 - 1319
 LEAK RATE, CFM: 0.000 0.000 TEST PERSONS: WAT

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH		FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@		XAD	WT.		
PITOT	✓	✓	<u>N22</u>	<u>09988</u>	<u>1.834</u>					
TC	✓	✓	PITOT ID <u>PT-7</u>	Cp <u>0.84</u>	METER TEMP. <u>70</u>		NA	NA		
NOZZLE	✓	✓	TC READOUT <u>Fuji</u>	TC <u>24</u>	EST. % H ₂ O <u>17</u>					
ORSAT	✓	NA	NOZZLE NO. <u>G292</u>	DIA. <u>0.217</u>	"C" FACTOR <u>0.755</u>					
			SAMPLE BOX <u>73</u>	REAGNT. <u>210</u>	STACK TEMP. <u>280</u>					
			UMBILICAL <u>U95</u>		REF DELTA-P <u>1.478</u>					
			ORSAT PUMP <u>OR1</u>	BAG <u>200</u>	"K" FACTOR <u>1.245</u>					

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

	PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	A-8	0	493.250	1.30	64	282	1.59	1.586	3	252	53	
2	7	2.5	495.073	1.36	65	282	1.66	1.659	3	240	50	
3	6	5.0	496.810	1.17	67	283	1.43	1.431	3	253	49	
	5	7.5	498.440	1.06	67	281	1.30	1.301	3	240	49	
	4	10.0	500.020	1.03	68	280	1.27	1.268	2	237	50	
6	3	12.5	501.350	0.97	69	279	1.198	1.198	2	248	50	
7	2	15.0	503.06	0.86	69	280	1.06	1.061	2	244	50	
8	1	17.5	504.457	0.65	70	272	0.81	0.813	2	247	51	
9	B-8	20.0	505.700	1.10	70	283	1.36	1.356	2	241	62	
10	7	22.5	507.385	1.10	70	285	1.35	1.350	2	235	63	
11	6	25.0	508.96	0.95	71	285	1.17	1.168	2	234	61	
12	5	27.5	510.485	0.98	71	282	1.21	1.209	2	248	58	
13	4	30.0	511.994	1.02	71	282	1.26	1.259	2	240	57	
14	3	32.5	513.588	1.00	71	278	1.24	1.241	2	235	57	
15	2	35.0	515.055	0.93	71	278	1.15	1.154	2	253	58	
16	1	37.5	516.520	0.65	71	268	0.82	0.818	2	252	58	
17	C-8	40.0	517.794	1.20	70	282	1.48	1.479	2	255	65	
18	7	42.5	519.620	1.18	71	282	1.46	1.455	2	241	56	
19	6	45.0	521.283	1.12	71	282	1.38	1.381	2	247	57	
20	5	47.5	522.910	1.15	71	283	1.42	1.417	2	244	56	
21	4	50.0	524.478	1.10	71	284	1.35	1.353	2	238	56	
22	3	52.5	526.08	1.26	72	287	1.55	1.55	2	248	59	
23	2	55.0	527.815	0.74	72	278	0.92	0.919	2	261	60	
	1	57.5	529.147	0.66	72	270	0.83	0.830	2	239	60	
	END	60.0	530.430									
	FINAL		37.18									

60 37.180 1.0125 7098 280.3 1.2613

REVIEWER SCG

31

SAMPLING DATA - METHOD (S) EPA101A

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, FC JOB NO.: 10382
 SAMPLE LOCATION: Unit 2 FFOutlet RUN NO.: 2-0-MIDIA-3
 BAR. PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: 216-146 DATE: 3/3/98
 LEAK ✓ VAC., IN. HG: 10 5 RUN TIME: 1344 - 1447
 LEAK RATE, CFM: 0.01 0.01 TEST PERSONS: WAT

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX		Y	DELTA H@			XAD	WT.	
PITOT	✓	✓	<u>N-22</u>		<u>0.9988</u>	<u>1.834</u>					
TC	✓	✓	PITOT ID		<u>Cp 0.84</u>	METER TEMP.	<u>70</u>		<u>NA</u>		
NOZZLE	✓	✓	TC READOUT	<u>Fuji</u>	<u>TC 49</u>	EST. % H ₂ O	<u>17</u>				
ORSAT	✓	NA	NOZZLE NO.	<u>6N</u>	DIA. <u>0.217</u>	"C" FACTOR	<u>0.755</u>				
			SAMPLE BOX	<u>64</u>	REAGNT. <u>210</u>	STACK TEMP.	<u>280</u>				
			UMBILICAL	<u>1195</u>		REF DELTA-P	<u>1.478</u>				
			ORSAT PUMP	<u>DR1</u>	BAG <u>B148</u>	"K" FACTOR	<u>1.235</u>				

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			<u>8%</u>

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-8	0.0	580.605	1.30	66	284	1.59	1.587	3	242	64	
2	7	25	532.515	1.30	66	282	1.55	1.589	3	240	58	
3	6	50	534.135	1.25	67	283	1.53	1.529	3	246	58	
4	5	75	535.815	1.30	67	283	1.59	1.590	3	239	58	
5	4	100	537.550	0.97	68	282	1.19	1.190	3	247	59	
6	3	125	539.055	0.94	68	283	1.15	1.163	3	247	60	
7	2	150	530.538	0.85	68	282	1.04	0.703	3	241	59	
8	1	175	541.937	0.56	69	268	0.7	0.703	3	246	58	
9	B-8	200	543.09	1.10	69	280	1.35	1.309	3	244	57	
10	7	225	544.800	0.94	69	279	1.16	1.161	3	248	56	
11	6	250	546.300	0.96	69	285	1.18	1.177	3	247	57	
12	5	275	547.725	1.08	70	285	1.23	1.228	3	241	57	
13	4	300	549.315	1.03	70	282	1.27	1.270	3	241	58	
14	3	325	550.870	1.05	70	283	1.30	1.297	3	247	58	
15	2	350	552.450	0.92	70	282	1.14	1.138	3	239	58	
16	1	375	553.918	0.60	70	269	0.76	0.756	3	244	59	
17	C-8	400	555.155	1.24	70	283	1.53	1.524	3	240	58	
18	7	425	556.980	1.23	70	284	1.52	1.517	3	242	56	
19	6	450	558.655	1.22	71	286	1.50	1.503	3	248	57	
20	5	475	560.330	1.15	71	286	1.42	1.417	3	240	57	
21	4	500	561.970	1.16	71	284	1.36	1.359	3	241	57	
22	3	525	563.	1.05	71	284	1.30	1.298	3	242	57	
23	2	550	565.137	0.62	71	279	0.77	0.772	3	240	58	
24	1	575	566.34	0.70	70	267	0.89	0.885	3	244	58	
25	END	60.0	567.700									

FINAL

REVIEWER

60 37095 10027 69.2 281.2 1.2529

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, OK JOB NO.: 10382
 PLE LOCATION: Unit 2 FF Outlet RUN NO.: 2-0-M101A-4
 BAR PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: -16.6 DATE: 3/3/98
 LEAK ✓ VAC., IN. HG: 12 6 RUN TIME: 1518 - 1622
 LEAK RATE, CFM: 0.000 0.006 TEST PERSONS: WAT

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	<u>N-22</u>	Y	<u>0.9988</u>	DELTA H@	<u>1.834</u>		XAD	WT.
PITOT	✓	✓	PITOT ID	<u>PT 7</u>	Cp	<u>0.84</u>	METER TEMP.	<u>70</u>		NA	NA
TC	✓	✓	TC READOUT	<u>Fuji</u>	TC		EST. % H ₂ O	<u>17</u>			
NOZZLE	✓	✓	NOZZLE NO.	<u>G292</u>	DIA.	<u>0.217</u>	"C" FACTOR	<u>0.735</u>			
ORSAT	✓	NA	SAMPLE BOX	<u>73</u>	REAGNT.	<u>57210700</u>	STACK TEMP.	<u>280</u>			
			UMBILICAL	<u>U95</u>			REF DELTA-P	<u>1.478</u>			
			ORSAT PUMP	<u>OR-1</u>	BAG	<u>B200</u>	"K" FACTOR	<u>1.245</u>			

LEAK CHECKS	B	B	B	B	FYRTES	%O ₂	%CO ₂	8% Bag	8% Bag
	E	E	E	E					

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-8	0	567.950	1.45	67	282	1.78	1.788	3	255	58	
2	7	2.5	564.880	1.35	67	284	1.65	1.623	3	243	57	
3	6	5.0	571.590	1.25	67	284	1.53	1.531	3	240	57	
	5	7.5	573.265	1.12	68	284	1.37	1.374	3	250	58	
	4	10.0	574.855	0.97	68	281	1.26	1.196	3	240	57	
6	3	12.5	576.355	0.94	69	282	1.16	1.160	3	249	57	
7	2	15.0	577.820	0.74	60	276	0.92	0.922	3	241	61	57
8	1	17.5	579.144	0.72	70	267	0.91	0.909	3	253	63	57
9	B-8	20.0	580.555	1.13	70	283	1.40	1.378	3	260	63	
10	7	22.5	582.240	1.00	70	283	1.23	1.234	3	241	62	
11	6	25.0	583.750	0.98	71	282	1.21	1.204	3	244	61	
12	5	27.5	585.250	1.00	71	283	1.23	1.232	3	241	60	
13	4	30.0	586.77	1.06	71	284	1.23	1.236	3	247	59	
14	3	32.5	588.302	1.15	72	283	1.42	1.419	4	252	59	
15	2	35.0	589.925	0.94	72	285	1.16	1.156	4	239	60	
16	1	37.5	591.370	0.7	72	275	0.87	0.873	4	244	64	
17	C-8	40.0	592.69	1.22	72	283	1.50	1.507	3	239	63	
18	7	42.5	594.350	1.25	72	288	1.53	1.531	3	261	63	
19	6	45.0	596.082	1.32	73	285	1.63	1.626	3	238	62	
20	5	47.5	597.825	1.26	74	288	1.475	1.475	3	250	62	
21	4	50.0	599.470	1.26	73	288	1.48	1.475	3	239	61	
22	3	52.5	601.125	1.13	74	288	1.39	1.389	3	243	61	
23	2	55.0	602.700	0.95	73	285	1.17	1.171	3	248	62	
		57.5	604.182	0.60	73	270	0.76	0.755	3	240	63	
		60.0	605.552									
FINAL			37602									

60 37.602 1.0431 70.8 282.3 1.3004 REVIEWER SCG

SAMPLING DATA - METHOD (S) Modified 101A

CLIENT: DODEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORLANDO, FL JOB NO.: 10382
 SAMPLE LOCATION: Unit 2 - FF Outlet RUN NO.: 2-0-MM101A-1
 BAR. PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: -16.1 DATE: 3/3/98
 LEAK VAC., IN. HG: 14 6 RUN TIME: 1655 - 1755
 LEAK RATE, CFM: 0.002 .000 TEST PERSONS: WAT / HOD

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	<u>N-22</u>	Y	<u>0.9988</u>	DELTA H@	<u>1.834</u>		XAD	WT.
PITOT	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	PITOT ID	<u>39</u>	Cp	<u>0.84</u>	METER TEMP.	<u>70</u>		NA	NA
TC	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	TC READOUT	<u>Fuji</u>	TC	<u>12</u>	EST. % H ₂ O	<u>17</u>			
NOZZLE	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	NOZZLE NO.	<u>G286</u>	DIA.	<u>0.217</u>	"C" FACTOR	<u>0.748</u>			
ORSAT	<input checked="" type="checkbox"/>	NA	SAMPLE BOX	<u>30</u>	REAGNT.	<u>C14/209</u>	STACK TEMP.	<u>280</u>			
			UMBILICAL	<u>U95</u>			REF DELTA-P	<u>1.490</u>			
			ORSAT PUMP	<u>OR1</u>	BAG	<u>B148</u>	"K" FACTOR	<u>1.235</u>			

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E		<u>8.8%</u>	<u>8.8%</u>

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP. °F	STACK TEMP. °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-8	0	605.800	1.36	68	284	1.67	1.667	3	243	64	
2	7	25	607.73	1.38	68	284	1.69	1.689	3	245	67	
3	6	50	609.51	1.20	68	288	1.46	1.460	3	239	657	
	5	75	611.70	1.05	69	290	1.28	1.278	3	239	55	
	4	100	612.710	1.03	70	288	1.26	1.260	3	247	65	
6	3	125	614.240	0.93	70	288	1.34	1.137	3	249	55	
7	2	150	615.710	0.90	70	283	1.11	1.108	3	249	55	
8	1	175	617.16	0.74	71	272	0.93	0.927	3	252	55	
9	B-8	200	618.535	1.10	70	284 275	1.36 1.36	1.363 1.363	3	246	58	
10	7	225	620.190	0.04	70	278	1.29	1.289	3	252	60	
11	6	250	621.740	0.94	71	284	1.16	1.158	3	244	60	
12	5	275	623.190	0.96	71	283	1.18	1.184	3	247	61	
13	4	300	624.675	1.05	71	285	1.28	1.272	3	241	61	
14	3	325	626.212	1.00	70	284	1.23	1.229	3	254	63	
15	2	350	627.725	0.94	70	284	1.16	1.156	3	257	63	
16	1	375	629.195	0.66	70	289	0.83	0.828	3	252	63	
17	C-8	400	630.45	1.26	68	280	1.55	1.55	3	253	64	
18	7	425	632.25	1.25	70	287	1.53	1.53	3	247	63	
19	6	450	633.88	1.19	70	290	1.45	1.45	3	256	63	
20	5	475	635.60	1.15	70	290	1.40	1.402	3	250	61	
21	4	500	637.235	1.07	70	289	1.31	1.306	3	251	61	
22	3	525	638.81	1.0	70	290	1.22	1.22	3	247	63	
23	2	550	640.36	0.85	69	287	1.04	1.039	3	254	64	
	1	575	641.80	1.02	70	281	1.26	1.260	3	248	64	
END		600	643.392									

FINAL 60 37.592 1.04 70 284 1.28 REVIEWER _____ 34

APPENDIX D

ANALYTICAL DATA

1.0 MOISTURE ANALYTICAL SHEETS

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10382

City / State OKAHUMPKA, FL Sampling Loc. _____

Run Number	<u>1-I-M101A-1</u>	<u>1-I-M101A-2</u>	<u>1-I-M101A-3</u>
Sampling Date	<u>3/4/98</u>	<u>3/4/98</u>	<u>3/4/98</u>
Analysis Date	<u>3/4/98</u>	<u>3/4/98</u>	<u>3/4/98</u>
Analyst	<u>HTD</u>	<u>HTD</u>	<u>HTD</u>

Reagent 1 (<u>KMnO4</u>)			
Final Weight, g	<u>616.7</u>	<u>704.7</u>	<u>700.0</u>
Tared Weight, g	<u>601.2</u>	<u>602.3</u>	<u>601.6</u>
Water Catch, g	<u>15.5</u>	<u>102.4</u>	<u>98.4</u>
Reagent 2 (_____)			
Final Weight, g	_____	_____	_____
Tared Weight, g	_____	_____	_____
Water Catch, g	_____	_____	_____
Reagent 3 (_____)			
Final Weight, g	_____	_____	_____
Tared Weight, g	_____	_____	_____
Water Catch, g	_____	_____	_____
CONDENSED WATER, g	<u>15.5</u>	<u>102.4</u>	<u>98.4</u>
Silica Gel			
Final Weight, g	<u>208.0</u>	<u>212.4</u>	<u>212.4</u>
Tared Weight, g	<u>200.0</u>	<u>200.0</u>	<u>200.0</u>
Water Catch, g	<u>8.0</u>	<u>12.4</u>	<u>12.4</u>
TOTAL WATER COLLECTED, g	<u>23.5</u>	<u>114.8</u>	<u>110.8</u>

Balance No. 2 Type Triple Beam Electronic Reagent Box 202

Balance located in stable, draft-free area (✓)? Yes No _____ (If "No," explain below.)

Comments balance in lab trailer D 2

FIELD SAMPLE RECOVERY QUALITY CONTROL

Box No. 202 Assembly Date 2/27/98 Assembled By G. MATA

Client OGDEN MARTIN SYSTEMS Job No. 10382

Plant OMS-LAKE City / State OKAHUMPLA

Sampling Location _____ Method _____

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Silca Gel 200 gm _____

Other (specify) _____

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS _____

D 3

RECORD OF CUSTODY, CONTAINER No. 202

Client OGDEN MARTIN SYSTEMS

Job No. 10382

Plant Name OMS - LAKE

City/State OKAHUMPKA, FL

Sampling Method (s) EPA 101A (EPA, NIOSH, etc.)

Container Type (v) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002874	2/27/98	2/27 1013	S	<i>[Signature]</i>	
	2/27/98	1055	B	<i>[Signature]</i>	Check Jars
	2/27/98	1105	S	<i>[Signature]</i>	
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact?***	
_____	_____	_____	Yes ___	No ___ N/A ___
Signature	Date	Time		

As Applicable:
All liquid levels at mark (v) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____

CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE

Job No. 10382

City / State OKAHUMPKA, FL

Sampling Loc. Unit # 1 FF Outle

Run Number	<u>1-0-M101A-4</u>	<u>1-I-M101A-4</u>	<u>1-0-M101A-5</u>
Sampling Date	<u>3/4/98</u>	<u>3/4/98</u>	<u>3/4/98</u>
Analysis Date	<u>3/4/98</u>	<u>3/4/98</u>	<u>3/4/98</u>
Analyst	<u>HTD</u>	<u>HTD</u>	<u>HTD</u>

<u>Reagent 1</u> (<u>KMnO4</u>)			
Final Weight, g	<u>721.2</u>	<u>704.1</u>	<u>725.4</u>
Tared Weight, g	<u>600.8</u>	<u>602.1</u>	<u>605.4</u>
Water Catch, g	<u>120.4</u>	<u>102.1</u>	<u>120.0</u>
<u>Reagent 2</u> (_____)			
Final Weight, g	_____	_____	_____
Tared Weight, g	_____	_____	_____
Water Catch, g	_____	_____	_____
<u>Reagent 3</u> (_____)			
Final Weight, g	_____	_____	_____
Tared Weight, g	_____	_____	_____
Water Catch, g	_____	_____	_____
CONDENSED WATER, g	<u>120.4</u>	<u>102.1</u>	<u>120.0</u>
<u>Silica Gel</u>			
Final Weight, g	<u>208.2</u>	<u>210.0</u>	<u>209.8</u>
Tared Weight, g	<u>200.0</u>	<u>200.0</u>	<u>200.0</u>
Water Catch, g	<u>8.2</u>	<u>10.0</u>	<u>9.8</u>
TOTAL WATER COLLECTED, g	<u>128.6</u>	<u>112.1</u>	<u>129.8</u>

Balance No. 2 Type (✓) Triple Beam Electronic _____ Reagent Box C10

Balance located in stable, draft-free area (✓)? Yes No _____ (If "No," explain below.)

Comments balance in lab trailer D 5

FIELD SAMPLE RECOVERY QUALITY CONTROL

Box No. C10 Assembly Date 2/27/98 Assembled By G. MATA

Client OGDEN MARTIN SYSTEMS Job No. 10382

Plant OMS-LAKE City / State OKAHUMPLA

Sampling Location _____ Method MOD. EPA 101A

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Silca Gel 200 gm _____

Other (specify) _____

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS _____ D 6

RECORD OF CUSTODY, CONTAINER No. C10

Client OGDEN MARTIN SYSTEMS

Job No. 10382

Plant Name OMS - LAKE

City/State OKAHUMPKA, FL

Sampling Method (s) MOD. EPA 101A (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002442	2/27/98	1017	S	<i>[Signature]</i>	
			B		
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **		
_____	_____	_____	Yes	No	N/A
Signature	Date	Time			

As Applicable:
 All liquid levels at mark (✓) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
 TUBE SAMPLES put in freezer by _____ Date _____ Time _____

CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name

OMS-LAKE

Job No.

10382

City / State

OKAHUMPKA, FL

Sampling Loc.

Unit #1 SPA Inlet

Run Number

1-I-m101A-5

Sampling Date

3/4/98

Analysis Date

3/4/98

Analyst

HTD

<u>Reagent 1</u> (<u>KMnO₄</u>)	Final Weight, g	<u>714.9</u>		
	Tared Weight, g	<u>605.8</u>		
	Water Catch, g	<u>109.1</u>		
<u>Reagent 2</u> (_____)	Final Weight, g			
	Tared Weight, g			
	Water Catch, g			
<u>Reagent 3</u> (_____)	Final Weight, g			
	Tared Weight, g			
	Water Catch, g			
CONDENSED WATER, g		<u>109.1</u>		
<u>Silica Gel</u>	Final Weight, g	<u>211.2</u>		
	Tared Weight, g	<u>200.0</u>		
	Water Catch, g	<u>11.2</u>		
TOTAL WATER COLLECTED, g		<u>120.3</u>		

Balance No.

2

Type (✓) Triple Beam

Electronic

Reagent Box

211

Balance located in stable, draft-free area (✓)?

Yes

No

(If "No," explain below.)

Comments

balance in lab trailer

D

8

RECORD OF CUSTODY, CONTAINER No. 211

Client OGDEN MARTIN SYSTEMS

Job No. 10382

Plant Name OMS - LAKE

City/State OKAHUMPKA, FL

Sampling Method (s) EPA 101A (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002192	2/27/98	1036	S	<i>[Signature]</i>	
			B		
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **	
_____	_____	_____	Yes ___	No ___ N/A ___
Signature	Date	Time		

As Applicable:
All liquid levels at mark (✓) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____

CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

FIELD SAMPLE RECOVERY QUALITY CONTROL

Box No. 211 Assembly Date 2/27/98 Assembled By G. MATA

Client OGDEN MARTIN SYSTEMS Job No. 10382

Plant OMS-LAKE City / State OKAHUMPLA

Sampling Location _____ Method _____

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Silca Gel 200 gm _____

Other (specify) _____

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS _____

D 10

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10382
 City/State OKAHUMPKA, FL Sampling Loc. UNIT No. 1

Run Number	<u>1-0-mm101A-1</u>	<u>1-I-mm101A-1</u>	
Sampling Date	<u>3/4/98</u>	<u>3/4/98</u>	
Analysis Date	<u>3/4/98</u>	<u>3/4/98</u>	
Analyst	<u>SCG</u>	<u>SCG</u>	

<u>Reagent 1 (0.1M KCl)</u>			
Final Weight, g	<u>387.3</u>	<u>372.9</u>	
Tared Weight, g	<u>259.0</u>	<u>258.8</u>	
Water Catch, g	<u>128.3</u>	<u>114.1</u>	
<u>Reagent 2 (0.1M KCl)</u>			
Final Weight, g	<u>149.1</u>	<u>148.1</u>	
Tared Weight, g	<u>142.3</u>	<u>142.0</u>	
Water Catch, g	<u>6.8</u>	<u>6.1</u>	
<u>Reagent 3 (4% KMnO4 / 10% H2SO4)</u>			
Final Weight, g	<u>609.3</u>	<u>610.6</u>	
Tared Weight, g	<u>602.5</u>	<u>601.6</u>	
Water Catch, g	<u>6.8</u>	<u>9.0</u>	
CONDENSED WATER, g	<u>141.9</u>	<u>129.2</u>	
<u>Silica Gel</u>			
Final Weight, g	<u>207.0</u>	<u>209.5</u>	
Tared Weight, g	<u>200.0</u>	<u>200.0</u>	
Water Catch, g	<u>7.10</u>	<u>9.5</u>	
TOTAL WATER COLLECTED, g	<u>148.9</u> ✓	<u>138.7</u> ✓	

Balance No. 2 Type (✓) Triple Beam Electronic Reagent Box 632
 Balance located in stable, draft-free area (✓)? Yes No (If "No," explain below.)

Comments _____

FIELD SAMPLE RECOVERY QUALITY CONTROL

Box No. 632 Assembly Date 2/27/98 Assembled By G. MATA

Client OGDEN MARTIN SYSTEMS Job No. 10382

Plant OMS-LAKE City / State OKAHUMPLA

Sampling Location UNIT Nos. 1 on Inlet & outlet Method Mod. fed 10 in

Individual Tare of Reagent 200 (ml) (gm) of 0.1M KCl

Individual Tare of Reagent 100 (ml) (gm) of 0.1M KCl

Individual Tare of Reagent 200 (ml) (gm) of 4% KMnO4 / 10% H2SO4

Individual Tare of Silca Gel 200 gm Other (specify) _____

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
1-0-mm101A-1	3/1/98	NA	NA	✓	SLG	3/4	30	✓	SLG
				Filter Appearance*					
				N/A					
				Reagent Appearance*					
				Clear / Purple					
1-I-mm101A-1	3/1	NA	NA	✓	SLG	3/4	30	✓	SLG
				Filter Appearance*					
				Heavy coating grey part.					
				Reagent Appearance*					
				Clear / Purple					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS _____

RECORD OF CUSTODY, CONTAINER No. 632

Client OGDEN MARTIN SYSTEMS

Job No. 10382

Plant Name OMS - LAKE

City/State OKAHUMPKA, FL

Sampling Method (s) MOD. EPA 101A (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002039	2/27/98	1133	S	<i>[Signature]</i>	
			B		
000246	3/4/98	2020	S	<i>[Signature]</i>	
			B		
	3/9/98	1153	S	<i>[Signature]</i>	log in samples
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **
<i>[Signature]</i>	<u>3/9/98</u>	<u>1153</u>	Yes <input checked="" type="checkbox"/> No <input type="checkbox"/> N/A <input type="checkbox"/>
Signature	Date	Time	

As Applicable:
All liquid levels at mark (✓) Yes No (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____
CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10382

City / State OKAHUMPKA, FL Sampling Loc. Unit #1 FF Outlet

Run Number	<u>1-0-M101A-1</u>	<u>1-0-M101A-2</u>	<u>1-0-M101A-3</u>
Sampling Date	<u>3/4/98</u>	<u>3/4/98</u>	<u>3/4/98</u>
Analysis Date	<u>3/4/98</u>	<u>3/4/98</u>	<u>3/4/98</u>
Analyst	<u>HTD</u>	<u>HTD</u>	<u>HTD</u>

<u>Reagent 1 (<u>KMnO4</u>)</u>			
Final Weight, g	<u>727.0</u>	<u>723.3</u>	<u>721.1</u>
Tared Weight, g	<u>603.2</u>	<u>600.2</u>	<u>603.1</u>
Water Catch, g	<u>123.8</u>	<u>123.1</u>	<u>118.0</u>
<u>Reagent 2 (_____)</u>			
Final Weight, g			
Tared Weight, g			
Water Catch, g			
<u>Reagent 3 (_____)</u>			
Final Weight, g			
Tared Weight, g			
Water Catch, g			
CONDENSED WATER, g	<u>123.8</u>	<u>123.1</u>	<u>118.0</u>
<u>Silica Gel</u>			
Final Weight, g	<u>210.6</u>	<u>210.1</u>	<u>211.4</u>
Tared Weight, g	<u>200.0</u>	<u>200.0</u>	<u>200.0</u>
Water Catch, g	<u>10.6</u>	<u>10.1</u>	<u>11.4</u>
TOTAL WATER COLLECTED, g	<u>124.4</u>	<u>133.2</u>	<u>129.4</u>

Balance No. 2 Type (✓) Triple Beam Electronic _____ Reagent Box 217

Balance located in stable, draft-free area (✓)? Yes No _____ (If "No," explain below.)

Comments Balance in lab trailer D 14

FIELD SAMPLE RECOVERY QUALITY CONTROL

Box No. 217 Assembly Date 2/27/98 Assembled By G. MATA
 Client OGDEN MARTIN SYSTEMS Job No. 10382
 Plant OMS-LAKE City / State OKAHUMPKA
 Sampling Location _____ Method _____

Individual Tare of Reagent _____ (ml) (gm) of _____
 Individual Tare of Reagent _____ (ml) (gm) of _____
 Individual Tare of Reagent _____ (ml) (gm) of _____
 Individual Tare of Silca Gel 200 gm _____
 Other (specify) _____

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS _____ 0 15

RECORD OF CUSTODY, CONTAINER No. 217

Client OGDEN MARTIN SYSTEMS

Job No. 10382

Plant Name OMS - LAKE

City/State OKAHUMPKA, FL

Sampling Method (s) EPA 101A (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002888	2/27/98	1034	S	<i>Shay M...</i>	
			B		
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **
_____	_____	_____	Yes ___ No ___ N/A ___
Signature	Date	Time	

As Applicable:
All liquid levels at mark (✓) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____

CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10382
 City / State OKAHUMPKA, FL Sampling Loc. Unit #2 SDA Inlet

Run Number	<u>2-I-M101A-1</u>	<u>2-I-M101A-2</u>	<u>2-I-M101A-3</u>
Sampling Date	<u>3/3/98</u>	<u>3/3/98</u>	<u>3/3/98</u>
Analysis Date	<u>3/3/98</u>	<u>3/3/98</u>	<u>3/3/98</u>
Analyst	<u>HTD</u>	<u>SCC</u>	<u>HTD</u>

<u>Reagent 1 (49% KMnO₄ / 10% H₂SO₄)</u>			
Final Weight, g	<u>734.4</u>	<u>722.5</u>	<u>724.0</u>
Tared Weight, g	<u>602.6</u>	<u>607.8</u>	<u>603.0</u>
Water Catch, g	<u>131.8</u>	<u>114.7</u>	<u>121.0</u>
<u>Reagent 2 (_____)</u>			
Final Weight, g	_____	_____	_____
Tared Weight, g	_____	_____	_____
Water Catch, g	_____	_____	_____
<u>Reagent 3 (_____)</u>			
Final Weight, g	_____	_____	_____
Tared Weight, g	_____	_____	_____
Water Catch, g	_____	_____	_____
CONDENSED WATER, g	<u>131.8</u>	<u>114.7</u>	<u>121.0</u>
<u>Silica Gel</u>			
Final Weight, g	<u>207.4</u>	<u>212.1</u>	<u>211.6</u>
Tared Weight, g	<u>200.0</u>	<u>200.0</u>	<u>200.0</u>
Water Catch, g	<u>7.4</u>	<u>12.1</u>	<u>11.6</u>
TOTAL WATER COLLECTED, g	<u>139.2</u>	<u>126.8</u>	<u>132.6</u>

Balance No. 2 Type Triple Beam Electronic _____ Reagent Box 205
 Balance located in stable, draft-free area (✓)? Yes No _____ (If "No," explain below)

Comments: Balance in lab trailer. D 17

FIELD SAMPLE RECOVERY QUALITY CONTROL

Box No. 205 Assembly Date 2/27/98 Assembled By G. MATA

Client OGDEN MARTIN SYSTEMS Job No. 10382

Plant OMS-LAKE City/State OKAHUMPKA

Sampling Location UNIT No. 2 INLET Method EPA 101A

Individual Tare of Reagent 200 (ml) (gm) of KMnO4

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Silca Gel 200 gm _____

Other (specify)

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
2-I-m101A-1	3/3/98	NA	NA	Y	HD	3/3/98	60	Y	HD
				Filter Appearance*					
				<u>dirty, inlet filter</u>					
				Reagent Appearance*					
				<u>ok</u>					
2-I-m101A-2	3/3/98	NA	NA	Y	HD	3/3/98	60	Y	HD
				Filter Appearance*					
				<u>same</u>					
				Reagent Appearance*					
				<u>ok</u>					
2-I-m101A-3	3/3/98	NA	NA	Y	HD	3/3/98	75	Y	HD
				Filter Appearance*					
				<u>same</u>					
				Reagent Appearance*					
				<u>ok</u>					
				Filter Appearance*					
				Reagent Appearance*					

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS _____

RECORD OF CUSTODY, CONTAINER No. 205

Client OGDEN MARTIN SYSTEMS

Job No. 10382

Plant Name OMS - LAKE

City/State OKAHUMPKA, FL

Sampling Method (s) EPA 101A (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002314	2/27/98	1019	S	<i>[Signature]</i>	To change trains
	3/2/98	1600	B		
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **		
_____	_____	_____	Yes	No	N/A
Signature	Date	Time			

As Applicable:
All liquid levels at mark (✓) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____
CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10382
 City/State OKAHUMPKA, FL Sampling Loc. Unit #2 SDA Inlet

Run Number 27-M101A-4
 Sampling Date 3/3/98
 Analysis Date 3/3/98
 Analyst HTD

Reagent 1 (<u>KMnO₄</u>)	Final Weight, g	<u>742.1</u>		
	Tared Weight, g	<u>606.5</u>		
	Water Catch, g	<u>135.6</u>		
Reagent 2 (_____)	Final Weight, g			
	Tared Weight, g			
	Water Catch, g			
Reagent 3 (_____)	Final Weight, g			
	Tared Weight, g			
	Water Catch, g			
CONDENSED WATER, g		<u>135.6</u>		
Silica Gel	Final Weight, g	<u>213.1</u>		
	Tared Weight, g	<u>200.0</u>		
	Water Catch, g	<u>13.1</u>		
TOTAL WATER COLLECTED, g		<u>148.7</u>		

Balance No. 2 Type Triple Beam Electronic _____ Reagent Box 204
 Balance located in stable, draft-free area (✓)? Yes No _____ (If "No," explain below.)
D 20

Comments Balance in lab trailer

FIELD SAMPLE RECOVERY QUALITY CONTROL

Box No. 204 Assembly Date 2/27/98 Assembled By G. MATA

Client OGDEN MARTIN SYSTEMS Job No. 10382

Plant OMS-LAKE City / State OKAHUMPLA

Sampling Location # 2 SDA Inlet Method EPA 101A

Individual Tare of Reagent 200 (ml) (~~gm~~) of KMnO4

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Silca Gel 200 gm

Other (specify)

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
<u>2-I MIDIA-4</u>	<u>3/3/98</u>	<u>NA</u>	<u>NA</u>	<u>Y</u>	<u>HD</u>	<u>3/3/98</u>	<u>75</u>	<u>Y</u>	<u>HD</u>
				Filter Appearance*					
				<u>ok, dirty</u>					
				Reagent Appearance*					
				<u>ok</u>					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS _____

RECORD OF CUSTODY, CONTAINER No. 204

Client OGDEN MARTIN SYSTEMS

Job No. 10382

Plant Name OMS - LAKE

City/State OKAHUMPKA, FL

Sampling Method (s) EPA ~~101A~~ ² (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002002	2/27/98	1028	S	<i>[Signature]</i>	
	3/3/98	1200	B	<i>[Signature]</i>	change train
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **	
_____	_____	_____	Yes ___	No ___ N/A ___
Signature	Date	Time		

As Applicable:
All liquid levels at mark (✓) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____

CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10382
 City / State OKAHUMPKA, FL Sampling Loc. Unit #2 SDA Inlet

Run Number 2-Immida-1
 Sampling Date 3/3/98
 Analysis Date 3/3/98
 Analyst HTD

<u>Reagent 1 (Imp 1+2 KCl)</u>	Final Weight, g	<u>380.5</u>			
	Tared Weight, g	<u>254.7</u>			
	Water Catch, g	<u>125.8</u>			
<u>Reagent 2 (Imp 3 KCl)</u>	Final Weight, g	<u>146.6</u>			
	Tared Weight, g	<u>142.5</u>			
	Water Catch, g	<u>4.1</u>			
<u>Reagent 3 (KMnO4)</u>	Final Weight, g	<u>607.6</u>			
	Tared Weight, g	<u>607.5</u>			
	Water Catch, g	<u>0.1</u>			
CONDENSED WATER, g		<u>130.0</u>			
<u>Silica Gel</u>	Final Weight, g	<u>210.0</u>			
	Tared Weight, g	<u>200.0</u>			
	Water Catch, g	<u>10.0</u>			
TOTAL WATER COLLECTED, g		<u>140.0</u> ✓			

Balance No. 2 Type (✓) Triple Beam Electronic Reagent Box 216
 Balance located in stable, draft-free area (✓)? Yes No (If "No," explain below)

Comments: balance in lab trailer D 23

Box No. 216

Assembly Date 2/27/98

Assembled By G. MATA

Client OGDEN MARTIN SYSTEMS

Job No. 10382

Plant OMS-LAKE

City / State OKAHUMPLA

Sampling Location Unit #2 SDA Inlet

Method EPA 101A

Individual Tare of Reagent 200 (ml) (gm) of Km₂O₄

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Silca Gel 200 gm

Other (specify)

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
<u>2-I-mm101A-1</u>	<u>3/3/98</u>	<u>NA</u>	<u>NA</u>	<u>Y</u>	<u>HD</u>	<u>3/3/98</u>	<u>50</u>	<u>Yes</u>	<u>HD</u>
				Filter Appearance*					
				<u>dirty, inlet filter</u>					
				Reagent Appearance*					
				<u>ok</u>					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS

RECORD OF CUSTODY, CONTAINER No. 216

Client OGDEN MARTIN SYSTEMS

Job No. 10382

Plant Name OMS - LAKE

City/State OKAHUMPKA, FL

Sampling Method (s) EPA 101A (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002053	2/27/98	1030	S	<i>[Signature]</i>	
	3/3/98	1230	B	<i>[Signature]</i>	change train
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **		
_____	_____	_____	Yes	No	N/A
Signature	Date	Time			

As Applicable:
All liquid levels at mark (✓) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____
CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10382
 City / State OKAHUMPKA, FL Sampling Loc. Unit #2 FF Outlet

Run Number 2-0-mm101A-1
 Sampling Date 3/3/98
 Analysis Date 3/3/98
 Analyst HTD

<u>Reagent 1 (Imp 1+2 KCl)</u>	Final Weight, g	<u>392.5</u>		
	Tared Weight, g	<u>258.8</u>		
	Water Catch, g	<u>133.7</u>		
<u>Reagent 2 (KMnO4)</u>	Final Weight, g	<u>605.2</u>		
	Tared Weight, g	<u>604.7</u>		
	Water Catch, g	<u>0.5</u>		
<u>Reagent 3 (Imp 3 KCl)</u>	Final Weight, g	<u>147.1</u>		
	Tared Weight, g	<u>141.5</u>		
	Water Catch, g	<u>5.6</u>		
CONDENSED WATER, g		<u>139.8</u>		
<u>Silica Gel</u>	Final Weight, g	<u>206.8</u>		
	Tared Weight, g	<u>200.0</u>		
	Water Catch, g	<u>6.8</u>		
TOTAL WATER COLLECTED, g		<u>146.6</u> ✓		

Balance No. 2 Type (✓) Triple Beam Electronic Reagent Box 209
 Balance located in stable, draft-free area (✓)? Yes No (If "No," explain below.)

Comments _____

FIELD SAMPLE RECOVERY QUALITY CONTROL

Box No. 209 Assembly Date 2/27/98 Assembled By G. MATA

Client OGDEN MARTIN SYSTEMS Job No. 10382

Plant OMS-LAKE City / State OKAHUMPKA

Sampling Location Unit # 2 FF outlet Method EPA 101A

Individual Tare of Reagent 200 (ml) (gm) of KMnO4

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Reagent _____ (ml) (gm) of _____

Individual Tare of Silca Gel 200 gm

Other (specify)

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
<u>2-D-MNH/1A-1</u>	<u>3/3/98</u>	<u>NA</u>	<u>NA</u>	<u>Y</u>	<u>HD</u>	<u>3/3/98</u>	<u>50</u>	<u>Y</u>	<u>HD</u>
				Filter Appearance*					
				<u>NA</u>					
				Reagent Appearance*					
				<u>OK</u>					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS

0 27

RECORD OF CUSTODY, CONTAINER No. 209

Client OGDEN MARTIN SYSTEMS

Job No. 10382

Plant Name OMS - LAKE

City/State OKAHUMPKA, FL

Sampling Method (s) EPA 101A (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002991	2/27/98	1032	S	<i>[Signature]</i>	
	3/3/98	1234	B	<i>[Signature]</i>	<i>change train</i>
0002373	3/4/98	2000	S	<i>[Signature]</i>	
	3/9/98	1149	B	<i>[Signature]</i>	<i>Reagent Samples</i>
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **
<i>[Signature]</i>	<u>3/9/98</u>	<u>1149</u>	Yes <input type="checkbox"/> No <input checked="" type="checkbox"/> N/A <input type="checkbox"/>
Signature	Date	Time	

As Applicable:
All liquid levels at mark (✓) Yes No (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____

CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10382
 City/State OKAHUMPKA, FL Sampling Loc. UNIT NO. 2 OUTLET

Run Number	<u>2-0-M101A-1</u>	<u>2-0-M101A-2</u>	<u>2-0-M101A3</u>
Sampling Date	<u>3/3/98</u>	<u>3/3/98</u>	<u>3/3/98</u>
Analysis Date	<u>3/3/98</u>	<u>3/3/98</u>	<u>3/3/98</u>
Analyst	<u>SCG</u>	<u>HTD</u>	<u>HTD</u>

<u>Reagent 1 (4.70% MnO₂ / 10.70% H₂SO₄)</u>			
Final Weight, g	<u>755.8</u>	<u>733.8</u>	<u>752.2</u>
Tared Weight, g	<u>600.4</u>	<u>605.7</u>	<u>605.2</u>
Water Catch, g	<u>155.4</u>	<u>128.1</u>	<u>147.0</u>
<u>Reagent 2 (_____)</u>			
Final Weight, g	_____	_____	_____
Tared Weight, g	_____	_____	_____
Water Catch, g	_____	_____	_____
<u>Reagent 3 (_____)</u>			
Final Weight, g	_____	_____	_____
Tared Weight, g	_____	_____	_____
Water Catch, g	_____	_____	_____
CONDENSED WATER, g	<u>155.4</u>	<u>128.1</u>	<u>147.0</u>
<u>Silica Gel</u>			
Final Weight, g	<u>214.3</u>	<u>212.5</u>	<u>210.5</u>
Tared Weight, g	<u>200.0</u>	<u>200.0</u>	<u>200.0</u>
Water Catch, g	<u>14.3</u>	<u>12.5</u>	<u>10.5</u>
TOTAL WATER COLLECTED, g	<u>169.7</u>	<u>140.6</u>	<u>157.5</u>

Balance No. 2 Type (✓) Triple Beam Electronic _____ Reagent Box 210
 Balance located in stable, draft-free area (✓)? Yes No _____ (If "No," explain below.)

Comments: Balance in lab trailer. D 29

Box No. 210 Assembly Date 2/27/98 Assembled By G. MATA
 Client OGDEN MARTIN SYSTEMS Job No. 10382
 Plant OMS-LAKE City / State OKAHUMPLA
 Sampling Location UNIT 2 OUTLET Method EPA 101A
 Individual Tare of Reagent 200 (ml) (gm) of KMnO4 / H2SO4
 Individual Tare of Reagent _____ (ml) (gm) of _____
 Individual Tare of Reagent _____ (ml) (gm) of _____
 Individual Tare of Silca Gel 200 gm _____

Other (specify)

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
2-0-m101A-1	3/3/98	NA	NA	Y	HD	3/3/98	75	Y	HD
				Filter Appearance*					
				<u>N/A</u>					
				Reagent Appearance*					
				<u>OK</u>					
2-0-m101A-2	3/3/98	NA	NA	Y	HD	3/3/98	80	Y	HD
				Filter Appearance*					
				<u>NA</u>					
				Reagent Appearance*					
				<u>h</u>					
2-0-m101A-3	3/3/98	NA	NA	Y	HD	3/3/98	50	Y	HD
				Filter Appearance*					
				<u>NA</u>					
				Reagent Appearance*					
				<u>h</u>					
				Filter Appearance*					
				Reagent Appearance*					

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS

D 30

RECORD OF CUSTODY, CONTAINER No. 210

Client OGDEN MARTIN SYSTEMS

Job No. 10382

Plant Name OMS - LAKE

City/State OKAHUMPKA, FL

Sampling Method (s) EPA 101A (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002110	2/27/98	1021	S	<i>[Signature]</i>	To change trains
	3/2/98	1555	B		
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **		
_____	_____	_____	Yes	No	N/A
Signature	Date	Time			

As Applicable:
All liquid levels at mark (✓) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____

CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10382
 City / State OKAHUMPKA, FL Sampling Loc. Outlet

Run Number 2-0-M101A-4
 Sampling Date 3/3/98
 Analysis Date 7HTD
 Analyst 3/3/98

Reagent 1 (<u>KMnO4</u>) Final Weight, g <u>758.8</u> Tared Weight, g <u>607.3</u> Water Catch, g <u>151.5</u>			
Reagent 2 (_____) Final Weight, g _____ Tared Weight, g _____ Water Catch, g _____			
Reagent 3 (_____) Final Weight, g _____ Tared Weight, g _____ Water Catch, g _____			
CONDENSED WATER, g	<u>151.5</u>		
Silica Gel Final Weight, g <u>210.8</u> Tared Weight, g <u>200.0</u> Water Catch, g <u>10.8</u>			
TOTAL WATER COLLECTED, g	<u>162.3</u>		

Balance No. 2 Type (✓) Triple Beam Electronic _____ Reagent Box 200
 Balance located in stable, draft-free area (✓)? Yes No _____ (If "No," explain below.)

Comments: balance in lab trailer. D 32

FIELD SAMPLE RECOVERY QUALITY CONTROL

Box No. 200 Assembly Date 2/27/98 Assembled By G. MATA
 Client OGDEN MARTIN SYSTEMS Job No. 10382
 Plant OMS-LAKE City / State OKAHUMPLA
 Sampling Location #2 FF outlet Method EPA 101A
 Individual Tare of Reagent 200 (ml) (gm) of KMnO4
 Individual Tare of Reagent _____ (ml) (gm) of _____
 Individual Tare of Reagent _____ (ml) (gm) of _____
 Individual Tare of Silca Gel 200 gm _____

Other (specify) _____

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
<u>2-0-1101A-4</u>	<u>3/3/98</u>	<u>NA</u>	<u>NA</u>	<u>Y</u>	<u>MD</u>	<u>3/3/98</u>	<u>50</u>	<u>Y</u>	<u>MD</u>
				Filter Appearance* <u>NA</u>					
				Reagent Appearance* <u>h</u>					
				Filter Appearance* _____					
				Reagent Appearance* _____					
				Filter Appearance* _____					
				Reagent Appearance* _____					
				Filter Appearance* _____					
				Reagent Appearance* _____					

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS _____ D 33

RECORD OF CUSTODY, CONTAINER No. 200

Client OGDEN MARTIN SYSTEMS

Job No. 10382

Plant Name OMS - LAKE

City/State OKAHUMPKA, FL

Sampling Method (s) EPA 101A (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002094	2/27/98	2/27/98	S	<i>Shay Mats</i>	<i>change trains</i>
	3/3/98	1200	B	<i>Nap Dileo</i>	
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **	
_____	_____	_____	Yes ___	No ___ N/A ___
Signature	Date	Time		

As Applicable:
All liquid levels at mark (✓) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____

CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

APPENDIX D

ANALYTICAL DATA

2.0 QUANTERRA ENVIRONMENTAL SERVICES

Quanterra Incorporated
880 Riverside Parkway
West Sacramento, California 95605

916 373-5600 Telephone
916 372-1059 Fax

March 10, 1998

QUANTERRA INCORPORATED PROJECT NUMBER: 097845
PO NUMBER: 664-SG Job #10382

Gary Mata
AirKinetics, Inc.
5932 Bolsa Avenue
Suite 105
Huntington Beach, CA 92649

Dear Mr. Mata:

This report contains the analytical results for the five airtrain samples which were received under chain of custody by Quanterra Incorporated on 05 March 1998.

The case narrative is an integral part of this report.

If you have any questions, please feel free to call.

Sincerely,



Robert Weidenfeld
Project Manager
Advanced Technology

RW/tr

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QUANTERRA INCORPORATED PROJECT NUMBER 097845

Case Narrative

Quanterra's Quality Assurance Program

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Chain of Custody Documentation

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Includes Sample: 1 through 5

Sample Data

Instrument Logs

Sample Preparation/Digestion Log Copies

CASE NARRATIVE

QUANTERRA INCORPORATED PROJECT NUMBER 097845

The results of the matrix spike and matrix spike duplicate were not calculated due to the high level of analyte in the sample compared to the spike concentration.

There were no additional anomalies associated with this report.

QUANTERRA INCORPORATED QUALITY CONTROL PROGRAM

Quanterra has implemented an extensive Quality Control (QC) program to ensure the production of scientifically sound, legally defensible data of known documentable quality. This QC program is based upon requirements in "Test Methods for Evaluating Solid Waste", USEPA SW-846, Third Edition. It applies whenever SW-846 analytical methods are used. It also applies in whole or in part whenever project requirements fail to specify some aspect of QC practices described here. It does not apply when other well defined QC programs (e.g. CLP or CLP-like) are specified. This is Quanterra's base QC program for environmental analysis.

Definitions:

Quality Control Batch. The quality control (QC) batch is a set of up to 20 field samples plus associated laboratory QC samples that are similar in composition (matrix) and that are processed within the same time period with the same reagent and standard lots.

Surrogate. A surrogate (or internal standard) is an organic compound similar in chemical behavior to the target analyte, but not normally found in environmental samples. Surrogates (or IS) are added to all samples in a batch to monitor the effects of both the matrix and the analytical process on accuracy.

Method Blank. A method blank (MB) is a control sample prepared using the same reagents used for the samples. As part of the QC batch, it accompanies the samples through all steps of the sample extraction and cleanup procedure. The method blank is used to monitor the level of contamination introduced to a batch of samples as a result of processing in the laboratory.

Laboratory Control Sample. A laboratory control sample (LCS) is prepared using a well characterized matrix (e.g., reagent water or Ottawa sand) that is spiked with known amounts of representative analytes. Alternate matrices (e.g., glass beads) may be used for soil analyses when Ottawa sand is not appropriate. As part of a QC batch, it accompanies the samples through all steps of the sample extraction and cleanup process. The LCS is used to monitor the accuracy of the analytical process independent of possible interference effects due to sample matrix.

Duplicate Control Sample. A duplicate laboratory control sample (DCS) consists of a pair of LCSs analyzed within the same QC batch to monitor precision and accuracy independent of sample matrix effects.

SAMPLE DESCRIPTION INFORMATION
for
AirKinetics, Inc.

Lab ID	Client ID	Matrix	Sampled Date	Time	Received Date
097845-0001-SA	1-I-M101A-4	AIRTRAIN	04	MAR 98	05 MAR 98
097845-0002-SA	1-I-M101A-5	AIRTRAIN	04	MAR 98	05 MAR 98
097845-0003-SA	1-O-M101A-4	AIRTRAIN	04	MAR 98	05 MAR 98
097845-0004-SA	1-O-M101A-5	AIRTRAIN	04	MAR 98	05 MAR 98
097845-0005-SA	1-O-M101A-FB	AIRTRAIN	04	MAR 98	05 MAR 98

Metals Emissions from Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-I-M101A-4
Lab ID: 097845-0001-SA
Matrix: AIRTRAIN
Authorized: 05 MAR 98

Sampled: 04 MAR 98
Prepared: See Below

Received: 05 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KMNO4	896	ug/Sample	40.0	7471	05 MAR 98	06 MAR 98 o
Mercury, HCL	16.7	ug/Sample	2.0	7471	06 MAR 98	06 MAR 98 o

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions from Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-I-M101A-5
Lab ID: 097845-0002-SA
Matrix: AIRTRAIN
Authorized: 05 MAR 98

Sampled: 04 MAR 98
Prepared: See Below

Received: 05 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KMNO4	462	ug/Sample	10.0	7471	05 MAR 98	06 MAR 98 o
Mercury, HCL	1.4	ug/Sample	0.10	7471	06 MAR 98	06 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions from Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-O-M101A-4
Lab ID: 097845-0003-SA
Matrix: AIRTRAIN
Authorized: 05 MAR 98

Sampled: 04 MAR 98
Prepared: See Below

Received: 05 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KMNO4	56.5	ug/Sample	2.0	7471	05 MAR 98	06 MAR 98 o
Mercury, HCL	0.24	ug/Sample	0.10	7471	06 MAR 98	06 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions from Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-0-M101A-5
Lab ID: 097845-0004-SA
Matrix: AIRTRAIN
Authorized: 05 MAR 98

Sampled: 04 MAR 98
Prepared: See Below

Received: 05 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KMNO4	55.5	ug/Sample	2.0	7471	05 MAR 98	06 MAR 98 o
Mercury, HCL	0.46	ug/Sample	0.10	7471	06 MAR 98	06 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions from Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-O-M101A-FB
Lab ID: 097845-0005-SA
Matrix: AIRTRAIN
Authorized: 05 MAR 98

Sampled: 04 MAR 98
Prepared: See Below

Received: 05 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KMNO4	ND	ug/Sample	0.20	7471	05 MAR 98	06 MAR 98
Mercury, HCL	ND	ug/Sample	0.10	7471	06 MAR 98	06 MAR 98

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
Rev 230787

QC LOT ASSIGNMENT REPORT - MS QC
Metals Analysis and Preparation

Laboratory Sample Number	QC Matrix	QC Category	QC Lot Number (DCS)	QC Run Number (SCS/BLANK/LCS)	MS QC Run Number (SA,MS,SD,DU)
097845-0001-SA	AQUEOUS	HG-TRC-G	05 MAR 98-T	05 MAR 98-T	05 MAR 98-TB
097845-0001-SA	AQUEOUS	HG-TRC-G	06 MAR 98-T	06 MAR 98-T	06 MAR 98-T
097845-0002-SA	AQUEOUS	HG-TRC-G	06 MAR 98-T	06 MAR 98-T	06 MAR 98-T
097845-0003-SA	AQUEOUS	HG-TRC-G	06 MAR 98-T	06 MAR 98-T	06 MAR 98-T
097845-0004-SA	AQUEOUS	HG-TRC-G	06 MAR 98-T	06 MAR 98-T	06 MAR 98-T
097845-0005-SA	AQUEOUS	HG-TRC-G	06 MAR 98-T	06 MAR 98-T	06 MAR 98-T

METHOD BLANK REPORT
Metals Analysis and Preparation

Analyte	Result	Units	Reporting Limit
---------	--------	-------	--------------------

Test: HG-CVAA-KMNO4-AIRTRA
Matrix: AIRTRAIN
QC Lot: 05 MAR 98-T QC Run: 05 MAR 98-T

Mercury, KMNO4	ND	ug/Sample	0.20
----------------	----	-----------	------

Test: HG-CVAA-HCL-AIRTRAIN
Matrix: AIRTRAIN
QC Lot: 06 MAR 98-T QC Run: 06 MAR 98-T

Mercury, HCL	ND	ug/Sample	0.20
--------------	----	-----------	------

DUPLICATE CONTROL SAMPLE REPORT
Metals Analysis and Preparation
Project: 097845

Category: HG-TRC-G Mercury analysis on air trains
 Testcode: HG-CVAA-KMNO4-AIRTRA Method: 7471
 Matrix: AQUEOUS Concentration Units: ug/L
 QC Lot: 05 MAR 98-T Analyzed Date: 05 MAR 98 Time: 17:32

Analyte	Spiked	-----Concentration-----			Accuracy Average(%)	Precision (RPD)		
		DCS1	DCS2	AVG				
Mercury, HCL	1.00	0.900	0.948	0.924	92	80-120	5.2	20
Mercury, KMNO4	1.00	0.900	0.948	0.924	92	80-120	5.2	20

Category: HG-TRC-G Mercury analysis on air trains
 Testcode: HG-CVAA-HCL-AIRTRAIN Method: 7471
 Matrix: AQUEOUS Concentration Units: ug/L
 QC Lot: 06 MAR 98-T Analyzed Date: 06 MAR 98 Time: 16:50

Analyte	Spiked	-----Concentration-----			Accuracy Average(%)	Precision (RPD)		
		DCS1	DCS2	AVG				
Mercury, HCL	1.00	1.03	1.04	1.03	103	80-120	0.6	20

Calculations are performed before rounding to avoid round-off errors in calculated results.

MATRIX SPIKE/MATRIX SPIKE DUPLICATE QC REPORT
Methods Analysis and Preparation
Project: 097845

Category: HG-TRC-G Mercury analysis on air trains
Test : HG-CVAA-KMNO4-AIRTRA
Matrix : AIRTRAIN
Sample : 097845-0001
MS Run : 05 MAR 98-TB
Units : ug/Sample

Method: 7471

Analyte	-----Concentration-----			Amount Spiked		%Recovery		%RPD	Acceptance Limit	
	Sample Result	MS Result	MSD Result	MS	MSD	MS	MSD		Recov.	RPD
Mercury, KMNO4	896 o	1010	1020	100	100	NC	NC	NC	80-120	20

o = Reporting limit(s) raised due to high level of analyte present in sample.
NC = Not Calculated, calculation not applicable.

Calculations are performed before rounding to avoid round-off errors in calculated results.

AirKinetics, Inc.

EMISSIONS CHARACTERIZATION AND TESTING SERVICES

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 664-SG JOB NAME: Ogden - Lake

LABORATORY: QUANTERRA JOB No.: 10382

DATE SAMPLES WERE TRANSMITTED: 4-Mar-98 EXPECTED DATE OF RESULTS: 9-Mar-98

SAMPLE MATRIX: 4% KMnO4/10% H2SO4

TYPE OF ANALYSIS REQUIRED: Please analyze according to EPA Method 101A for Hg only.

Sample / Run ID #	Sample Collection Date	Sample Components	Sample Matrix	Condition of Samples *
I-I-M101A-4	3/4/98	KMnO4	KMnO4/H2SO4	(w/filter)
	3/4/98	HCl	25 ml HCl in DI	
I-I-M101A-5	3/4/98	KMnO4	KMnO4/H2SO4	(w/filter)
	3/4/98	HCl	25 ml HCl in DI	
I-O-M101A-4	3/4/98	KMnO4	KMnO4/H2SO4	
	3/4/98	HCl	25 ml HCl in DI	
I-O-M101A-5	3/4/98	KMnO4	KMnO4/H2SO4	
	3/4/98	HCl	25 ml HCl in DI	
I-O-M101A-FB	3/4/98	KMnO4	KMnO4/H2SO4	
		HCl	25 ml HCl in DI	

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: Shawn Graham Date/Time: 3/4/98

Transported by: FedEx Date/Time: 3/4/98

Transported to: Quanterra Environmental Services
880 Riverside Parkway
West Sacramento, CA 95605-1501

Received by: *[Signature]* Date/Time: 030598 10:20

Quanterra Incorporated
880 Riverside Parkway
West Sacramento, California 95605

916 373-5600 Telephone
916 372-1059 Fax

March 13, 1998

QUANTERRA INCORPORATED PROJECT NUMBER: 097818
PO NUMBER: 664-SG Job #10382

Gary Mata
AirKinetics, Inc.
5932 Bolsa Avenue
Suite 105
Huntington Beach, CA 92649

Dear Mr. Mata:

This report contains the analytical results for the five airtrain samples which were received under chain of custody by Quanterra Incorporated on 04 March 1998.

The case narrative is an integral part of this report.

If you have any questions, please feel free to call.

Sincerely,



Robert Weidenfeld
Project Manager
Advanced Technology

RW/rr

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QUANTERRA INCORPORATED PROJECT NUMBER 097818

Case Narrative

Quanterra's Quality Assurance Program

Sample Description Information

Chain of Custody Documentation

Summary Report

Metals Emissions from Stationary Sources - Method 101A

Includes Sample: 1 through 5

Sample Data

Instrument Logs

Sample Preparation/Digestion Log Copies

CASE NARRATIVE

QUANTERRA INCORPORATED PROJECT NUMBER 097818

There were no anomalies associated with this report.

QUANTERRA INCORPORATED QUALITY CONTROL PROGRAM

Quanterra has implemented an extensive Quality Control (QC) program to ensure the production of scientifically sound, legally defensible data of known documentable quality. This QC program is based upon requirements in "Test Methods for Evaluating Solid Waste", USEPA SW-846, Third Edition. It applies whenever SW-846 analytical methods are used. It also applies in whole or in part whenever project requirements fail to specify some aspect of QC practices described here. It does not apply when other well defined QC programs (e.g. CLP or CLP-like) are specified. This is Quanterra's base QC program for environmental analysis.

Definitions:

Quality Control Batch. The quality control (QC) batch is a set of up to 20 field samples plus associated laboratory QC samples that are similar in composition (matrix) and that are processed within the same time period with the same reagent and standard lots.

Surrogate. A surrogate (or internal standard) is an organic compound similar in chemical behavior to the target analyte, but not normally found in environmental samples. Surrogates (or IS) are added to all samples in a batch to monitor the effects of both the matrix and the analytical process on accuracy.

Method Blank. A method blank (MB) is a control sample prepared using the same reagents used for the samples. As part of the QC batch, it accompanies the samples through all steps of the sample extraction and cleanup procedure. The method blank is used to monitor the level of contamination introduced to a batch of samples as a result of processing in the laboratory.

Laboratory Control Sample. A laboratory control sample (LCS) is prepared using a well characterized matrix (e.g., reagent water or Ottawa sand) that is spiked with known amounts of representative analytes. Alternate matrices (e.g., glass beads) may be used for soil analyses when Ottawa sand is not appropriate. As part of a QC batch, it accompanies the samples through all steps of the sample extraction and cleanup process. The LCS is used to monitor the accuracy of the analytical process independent of possible interference effects due to sample matrix.

Duplicate Control Sample. A duplicate laboratory control sample (DCS) consists of a pair of LCSs analyzed within the same QC batch to monitor precision and accuracy independent of sample matrix effects.

SAMPLE DESCRIPTION INFORMATION
for
AirKinetics, Inc.

Lab ID	Client ID	Matrix	Sampled Date	Time	Received Date
097818-0001-SA	2-I-M101A-1	AIRTRAIN	03 MAR 98		04 MAR 98
097818-0001-MS	2-I-M101A-1	AIRTRAIN	03 MAR 98		04 MAR 98
097818-0001-SD	2-I-M101A-1	AIRTRAIN	03 MAR 98		04 MAR 98
097818-0002-SA	2-I-M101A-2	AIRTRAIN	03 MAR 98		04 MAR 98
097818-0003-SA	2-O-M101A-1	AIRTRAIN	03 MAR 98		04 MAR 98
097818-0004-SA	2-O-M101A-2	AIRTRAIN	03 MAR 98		04 MAR 98
097818-0005-SA	Reagent Blank	AIRTRAIN	03 MAR 98		04 MAR 98

Metals Emissions from Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 2-I-M101A-1
Lab ID: 097818-0001-SA
Matrix: AIRTRAIN
Authorized: 04 MAR 98

Sampled: 03 MAR 98
Prepared: See Below
Received: 04 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KMNO4	35.5	ug/Sample	4.0	7471	04 MAR 98	04 MAR 98 o
Mercury, HCL	1.7	ug/Sample	0.10	7471	05 MAR 98	05 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions from Stationary Sources

Client Name: AirKinetics, Inc.
 Client ID: 2-I-M101A-2
 Lab ID: 097818-0002-SA
 Matrix: AIRTRAIN
 Authorized: 04 MAR 98

Sampled: 03 MAR 98
 Prepared: See Below

Received: 04 MAR 98
 Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KMNO4	128	ug/Sample	4.0	7471	04 MAR 98	04 MAR 98 o
Mercury, HCL	3.1	ug/Sample	0.10	7471	05 MAR 98	05 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
 NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
 Rev 230787

Metals Emissions from Stationary Sources

Client Name: AirKinetics, Inc.
 Client ID: 2-O-M101A-1
 Lab ID: 097818-0003-SA
 Matrix: AIRTRAIN
 Authorized: 04 MAR 98

Sampled: 03 MAR 98
 Prepared: See Below

Received: 04 MAR 98
 Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KMNO4	0.51	ug/Sample	0.20	7471	04 MAR 98	04 MAR 98
Mercury, HCL	0.28	ug/Sample	0.10	7471	05 MAR 98	05 MAR 98

ND = Not detected
 NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
 Rev 230787

Metals Emissions from Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 2-O-M101A-2
Lab ID: 097818-0004-SA
Matrix: AIRTRAIN
Authorized: 04 MAR 98

Sampled: 03 MAR 98
Prepared: See Below

Received: 04 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KMNO4	5.3	ug/Sample	0.20	7471	04 MAR 98	04 MAR 98
Mercury, HCL	0.33	ug/Sample	0.10	7471	05 MAR 98	05 MAR 98

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions from Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: Reagent Blank
Lab ID: 097818-0005-SA
Matrix: AIRTRAIN
Authorized: 04 MAR 98

Sampled: 03 MAR 98
Prepared: See Below

Received: 04 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KMNO4	ND	ug/Sample	0.20	7471	04 MAR 98	04 MAR 98
Mercury, HCL	ND	ug/Sample	0.10	7471	05 MAR 98	05 MAR 98

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
Rev 230787

QC LOT ASSIGNMENT REPORT - MS QC
 Metals Analysis and Preparation

Laboratory Sample Number	QC Matrix	QC Category	QC Lot Number (DCS)	QC Run Number (SCS/BLANK/LCS)	MS QC Run Number (SA,MS,SD,DU)
097818-0001-MS	AQUEOUS	HG-TRC-G	04 MAR 98-T	04 MAR 98-T	04 MAR 98-T
097818-0001-MS	AQUEOUS	HG-TRC-G	05 MAR 98-T	05 MAR 98-T	05 MAR 98-T
097818-0001-SA	AQUEOUS	HG-TRC-G	04 MAR 98-T	04 MAR 98-T	04 MAR 98-T
097818-0001-SA	AQUEOUS	HG-TRC-G	05 MAR 98-T	05 MAR 98-T	05 MAR 98-T
097818-0001-SD	AQUEOUS	HG-TRC-G	04 MAR 98-T	04 MAR 98-T	04 MAR 98-T
097818-0001-SD	AQUEOUS	HG-TRC-G	05 MAR 98-T	05 MAR 98-T	05 MAR 98-T

METHOD BLANK REPORT
Metals Analysis and Preparation

Analyte	Result	Units	Reporting Limit
Test: HG-CVAA-KMNO4-AIRTRA Matrix: AIRTRAIN QC Lot: 04 MAR 98-T QC Run: 04 MAR 98-T			
Mercury, KMNO4	ND	ug/Sample	0.20
Test: HG-CVAA-HCL-AIRTRAIN Matrix: AIRTRAIN QC Lot: 05 MAR 98-T QC Run: 05 MAR 98-T			
Mercury, HCL	ND	ug/Sample	0.20
Test: HG-CVAA-KMNO4-AIRTRA Matrix: AIRTRAIN QC Lot: 04 MAR 98-T QC Run: 04 MAR 98-T			
Mercury, KMNO4	ND	ug/Sample	0.20
Test: HG-CVAA-HCL-AIRTRAIN Matrix: AIRTRAIN QC Lot: 05 MAR 98-T QC Run: 05 MAR 98-T			
Mercury, HCL	ND	ug/Sample	0.20

DUPLICATE CONTROL SAMPLE REPORT
Metals Analysis and Preparation

Analyte	Concentration Spiked	Concentration Measured		AVG	Accuracy Average (%)		Precision (RPD)
		DCS1	DCS2		DCS	Limits	DCS Limit
Category: HG-TRC-G							
Matrix: AQUEOUS							
QC Lot: 04 MAR 98-T							
Concentration Units: ug/L							
Mercury	1.0	NA	NA	NC	NC	80-120	NC 20.0
Mercury, BH	1.0	NA	NA	NC	NC	80-120	NC 20.0
Mercury, Condensate	1.0	NA	NA	NC	NC	80-120	NC 20.0
Mercury, FH	1.0	NA	NA	NC	NC	80-120	NC 20.0
Mercury, FHBH	1.0	NA	NA	NC	NC	80-120	NC 20.0
Mercury, HCL	1.0	NA	NA	NC	NC	80-120	NC 20.0
Mercury, KMNO4	1.0	1.06	1.08	1.07	107	80-120	1.4 20.0

Category: HG-TRC-G
Matrix: AQUEOUS
QC Lot: 05 MAR 98-T
Concentration Units: ug/L

Mercury	1	NA		NC	NC	80-120	NC 20.0
Mercury, BH	1.0	NA		NC	NC	80-120	NC 20.0
Mercury, Condensate	1.0	NA		NC	NC	80-120	NC 20.0
Mercury, FH	1.0	NA		NC	NC	80-120	NC 20.0
Mercury, FHBH	1.0	NA		NC	NC	80-120	NC 20.0
Mercury, HCL	1.0	0.900	0.948	0.924	92	80-120	5.2 20.0
Mercury, KMNO4	1.0	0.900	0.948	0.924	92	80-120	5.2 20.0

The analyte was positively identified, the quantitation is an estimation.

NC = Not calculated, calculation not applicable.

The data are unusable due to deficiencies in the ability to analyze the sample and meet QC criteria.

Calculations are performed before rounding to avoid round-off errors in calculated results.

IX SPIKE/MATRIX SPIKE DUPLICATE QC REPORT
Metals Analysis and Preparation
Project: 097818

Category: HG-TRC-G Mercury analysis on air trains
Test : HG-CVAA-KMNO4-AIRTRA
Matrix : AIRTRAIN
Sample : 097818-0001
MS Run : 04 MAR 98-T
Units : ug/Sample

Method: 7471

Analyte	-----Concentration-----			Amount Spiked		%Recovery		%RPD	Acceptance Limit Recov. RPD
	Sample Result	MS Result	MSD Result	MS	MSD	MS	MSD		
Mercury, KMNO4	35.5 o	138	139	100	100	102	104	1.0	80-120 20

Category: HG-TRC-G Mercury analysis on air trains
Test : HG-CVAA-HCL-AIRTRAIN
Matrix : AIRTRAIN
Sample : 097818-0001
MS Run : 05 MAR 98-T
Units : ug/Sample

Method: 7471

Analyte	-----Concentration-----			Amount Spiked		%Recovery		%RPD	Acceptance Limit Recov. RPD
	Sample Result	MS Result	MSD Result	MS	MSD	MS	MSD		
Mercury, HCL	1.67	50.8 o	52.9	o 50.0	50.0	98	102	4.1	80-120 20

o Reporting limit(s) raised due to high level of analyte present in sample.

Calculations are performed before rounding to avoid round-off errors in calculated results.

AirKinetics, Inc.

EMISSIONS CHARACTERIZATION AND TESTING SERVICES

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 664-SG JOB NAME: Ogden - Lake

LABORATORY: QUANTERRA JOB No.: 10382

DATE SAMPLES WERE TRANSMITTED: 3-Mar-98 EXPECTED DATE OF RESULTS: 6-Mar-98

SAMPLE MATRIX: 4% KMnO4/10% H2SO4

TYPE OF ANALYSIS REQUIRED: Please analyze according to EPA Method 101A for Hg only.

Sample / Run ID #	Sample Collection Date	Sample Components	Sample Matrix	Condition of Samples *
2-I-M101A-1	3/3/98	KMnO4	KMnO4/H2SO4	(w/filter)
	3/3/98	HCl	25 ml HCl in DI	
2-I-M101A-2	3/3/98	KMnO4	KMnO4/H2SO4	(w/filter)
	3/3/98	HCl	25 ml HCl in DI	
2-O-M101A-1	3/3/98	KMnO4	KMnO4/H2SO4	
	3/3/98	HCl	25 ml HCl in DI	
2-O-M101A-2	3/3/98	KMnO4	KMnO4/H2SO4	
	3/3/98	HCl	25 ml HCl in DI	
Reagent Blank	3/3/98	KMnO4	KMnO4/H2SO4	
		HCl	25 ml HCl in DI	

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: Shawn Graham Date/Time: 3/3/98

Transported by: FedEx Date/Time: 3/3/98

Transported to: Quanterra Environmental Services
880 Riverside Parkway
West Sacramento, CA 95605-1501

Received by: *[Signature]* Date/Time: 03/04/98 *10:20*

put in good condition.

APPENDIX D

ANALYTICAL DATA

3.0 PHILIP ANALYTICAL SERVICES CORPORATION



**MERCURY DATA PACKAGE
FOR
AIR KINETICS INC.
Project # OMS - Lake**

**Philip Analytical Services
5555 North Service Road
Burlington, Ontario L7L 5H7**

Submission #8C0132 & 8C0095

Prepared by: Colin McGandy - CSR
Approved by : Dr. Ron McLeod - Principal Scientist

Initial : CM
Initial : Rm

D 67

000001

1. CASE NARRATIVE

PROJECT NARRATIVE

PHILIP Analytical Services (Burlington ON)

Philip Project: AN980186

Philip Submission #:8C0093

Client: Air Kinetics, Inc.

Client Project: 10382

I. SAMPLE RECEIPT/ANALYSIS

a) Sample Listing

Philip ID ON.	Client Sample ID	Date Sampled	Date Received	Date Prepped	Run Date
<i>Mercury A1 via 101A-A1</i>					
009245 98	Method Blank	98/03/03	98/03/04	98/03/04	98/03/05
009246 98	2-I-M101A-3	98/03/03	98/03/04	98/03/04	98/03/05
009247 98	2-I-M101A-4	98/03/03	98/03/04	98/03/04	98/03/05
009248 98	2-O-M101A-3	98/03/03	98/03/04	98/03/04	98/03/05
009249 98	2-O-M101A-4	98/03/03	98/03/04	98/03/04	98/03/05
009250 98	Reagent Blank	98/03/03	98/03/04	98/03/04	98/03/05
009540 98	Method Blank	98/03/04	98/03/05	98/03/05	98/03/06
009541 98	1-I-M101A-2	98/03/04	98/03/05	98/03/05	98/03/06
009542 98	1-I-M101A-3	98/03/04	98/03/05	98/03/05	98/03/06
009543 98	1-O-M101A-2	98/03/04	98/03/05	98/03/05	98/03/06
009544 98	1-O-M101A-3	98/03/04	98/03/05	98/03/05	98/03/06
009545 98	2-O-M101A-FB	98/03/04	98/03/05	98/03/05	98/03/06
<i>Mercury A1 via 101A-A2</i>					
009245 98	Method Blank	98/03/03	98/03/04	98/03/05	98/03/06
009246 98	2-I-M101A-3	98/03/03	98/03/04	98/03/05	98/03/06
009247 98	2-I-M101A-4	98/03/03	98/03/04	98/03/05	98/03/06
009248 98	2-O-M101A-3	98/03/03	98/03/04	98/03/05	98/03/06
009249 98	2-O-M101A-4	98/03/03	98/03/04	98/03/05	98/03/06
009250 98	Reagent Blank	98/03/03	98/03/04	98/03/05	98/03/06
009540 98	Method Blank	98/03/04	98/03/05	98/03/06	98/03/06
009541 98	1-I-M101A-2	98/03/04	98/03/05	98/03/06	98/03/06
009542 98	1-I-M101A-3	98/03/04	98/03/05	98/03/06	98/03/06
009543 98	1-O-M101A-2	98/03/04	98/03/05	98/03/06	98/03/06
009544 98	1-O-M101A-3	98/03/04	98/03/05	98/03/06	98/03/06
009545 98	2-O-M101A-FB	98/03/04	98/03/05	98/03/06	98/03/06

Run Date is defined as the date of injection of the last calibration standard (12 hour or less) prior to the samples analyzed within that run sequence. Therefore the time of calibration injection that defines the run date is always within 12 hours of the time of sample injection.

- b) Shipping Problems: none encountered
- c) Documentation Problems: none encountered

II. SAMPLE PREP:

No problems encountered

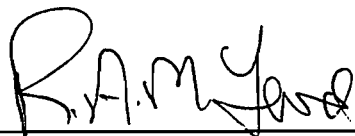
III. SAMPLE ANALYSIS:

See also comments within the appropriate Certificate of Analysis.

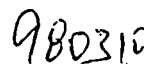
- a) Hold Times: all within recommended hold times
- b) Instrument Calibration: all within control limits
- c) Surrogate/Internal Recoveries: except where noted otherwise, all within control limits

I certify that this data package is in compliance with the terms and conditions of the contract, both technically and for completeness, for other than the conditions detailed above.

In addition, I certify, that to the best of my knowledge and belief, the data as reported are true and accurate. Release of the data contained in this data package has been authorized by the cognizant laboratory official or his/her designee, as verified by this signature.



Ronald A. McLeod, Principal Sci. Ph.D., C.Chem.



Date

000004

2. ANALYTICAL DATA REPORT

Certificate of Analysis

CLIENT INFORMATION

Attention: Shawn Graham
Client Name: Air Kinetics, Inc.
Project: 10382
Project Desc: OMS - Lake

Address: 5932 Bolsa Avenue, Suite 105
Huntington Beach, CA
CA 92649

Fax Number: 714 895 1915
Phone Number: 714 373 0998

LABORATORY INFORMATION

Contact: Ron McLeod
Project: AN980186
Date Received: 98/03/04
Date Reported: 98/03/08

Submission No.: 8C0132
Sample No.: 009245-009545

NOTES: *''.' = not analysed '<' = less than Method Detection Limit (MDL) 'NA' = no data available*
LOQ can be determined for all analytes by multiplying the appropriate MDL X 3.33
Solids data is based on dry weight except for biota analyses.
Organic analyses are not corrected for extraction recovery standards except for isotope dilution methods, (i.e. CARB 429 PAH, all PCDD/F and DBD/DBF analyses)

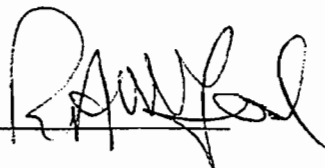
Methods used by PASC are based upon those found in 'Standard Methods for the Examination of Water and Wastewater', Seventeenth Edition. Other methods are based on the principles of MISA or EPA methodologies. New York State: ELAP Identification Number 10756.

All work recorded herein has been done in accordance with normal professional standards using accepted testing methodologies, quality assurance and quality control procedures except where otherwise agreed to by the client and testing company in writing. Any and all use of these test results shall be limited to the actual cost of the pertinent analysis done. There is no other warranty expressed or implied. Your samples will be retained at PASC for a period of three weeks from receipt of data or as per contract.

COMMENTS:

- * Sample concentration(s) too high to differentiate spike
- ** Loss of approximately 10% of the sample during transportation. The volume lost was estimated by the volume retained within the sealed plastic bag in which the sample bottle was shipped. The bottles were double bagged and there was no significant leakage from the first bag into the second bag. The analytical data are from the contents of the bottle only. No correction has been made for the loss of solution.

Certified by:



PASC - Certificate of Analysis

Component	MDL	Units	Method	Blank	Blank	Blank	Blank	2	2	2	2	2	2	
			Blank #1	Spike #1	Spike #1	Spike #2	Spike #2	I-M101A-3	I-M101A-3	I-M101A-3	I-M101A-3	I-M101A-3	I-M101A-3	
			009245 98	009245 98	009245 98	009245 98	009245 98	009246 98	009246 98	009246 98	009246 98	009246 98	009246 98	
			-	-	-	-	-	98/03/03	98/03/03	98/03/03	98/03/03	98/03/03	98/03/03	
					% Recoveries		% Recoveries		Duplicate		M. Spike	MS % Rec.	MS Dup	MSD % Rec.
Mercury (A1)	0.050	ug	<0.10	1.0	100	1.0	100	100	97	190	89	180	84	
Mercury (A2)	0.050	"	<	0.53	110	0.51	100	4.1	4.1	4.8	130*	4.6	96*	

D 73

000006

Component	MDL	Units	2	2	2	Reagent
			I-M101A-4	O-M101A-3	O-M101A-4	Blank
			009247 98	009248 98	009249 98	009250 98
			98/03/03	98/03/03	98/03/03	98/03/03
Mercury (A1)	0.050	ug	88	5.5	6.2	<0.10**
Mercury (A2)	0.050	"	3.7	0.078	<	<

D 74

000007

PASC - Certificate of Analysis

Component	MDL	Units	Method	Blank	Blank	Blank	Blank	1	1	1	1	1	1
			Blank #2	Spike #3	Spike #3	Spike #4	Spike #4	I-M101A-2	I-M101A-2	I-M101A-2	I-M101A-2	I-M101A-2	I-M101A-2
			009540 98	009540 98	009540 98	009540 98	009540 98	009541 98	009541 98	009541 98	009541 98	009541 98	009541 98
			-	-	-	-	-	98/03/04	98/03/04	98/03/04	98/03/04	98/03/04	98/03/04
					% Recoveries		% Recoveries		Duplicate	M. Spike	MS % Rec.	MS Dup	MSD % Rec.
Mercury (A1)	0.050	ug	<0.10	1.0	100	1.0	110	1100	1100	2100	97	2000	89
Mercury (A2)	0.050	"	<	0.56	110	0.53	110	14	13	23	100	24	100

0 75

800000

PASC - Certificate of Analysis

			1	1	1	2
Client ID:			I-M101A-3	O-M101A-2	O-M101A-3	O-M101A-FB
Lab No.:			009542 98	009543 98	009544 98	009545 98
Date Sampled:			98/03/04	98/03/04	98/03/04	98/03/04
Component	MDL	Units				
Mercury (A1)	0.050	ug	1400	46	61	<0.10**
Mercury (A2)	0.050	"	11	0.079	<0.25	<

D 76

600009

Batch Code:	03041SA1	03051SA1
Mercury (A1)	009245 98	009540 98
	009246 98	009541 98
	009247 98	009542 98
	009248 98	009543 98
	009249 98	009544 98
	009250 98	009545 98
Run Date	98/03/05	98/03/06
Date of Sample Prep	98/03/04	98/03/05

Batch Code:	03052SA2	03061GA2
Mercury (A2)	009245 98	009540 98
	009246 98	009541 98
	009247 98	009542 98
	009248 98	009543 98
	009249 98	009544 98
	009250 98	009545 98
Run Date	98/03/06	98/03/06
Date of Sample Prep	98/03/05	98/03/06

4. SHIPPING/RECEIVING DOCUMENTS

Chain-of-Custody Records

Miscellaneous Shipping/Receiving Records (describe or list)

EMISSIONS CHARACTERIZATION AND TESTING SERVICES

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 665-SG JOB NAME: Ogden - Lake

LABORATORY: Phillip JOB No.: 10382

DATE SAMPLES WERE TRANSMITTED: 4-Mar-98 EXPECTED DATE OF RESULTS: 9-Mar-98

SAMPLE MATRIX: 4% KMnO4/10% H2SO4

TYPE OF ANALYSIS REQUIRED: Please analyze according to EPA Method 101A for Hg only.

Sample / Run ID #	Sample Collection Date	Sample Components	Sample Matrix	Condition of Samples *
1-I-M101A-2	3/4/98	KMnO4	KMnO4/H2SO4	(w/filter) 1, 5002/
	3/4/98	HCl	25 ml HCl in DI	
1-I-M101A-3	3/4/98	KMnO4	KMnO4/H2SO4	(w/filter) "
	3/4/98	HCl	25 ml HCl in DI	
1-O-M101A-2	3/4/98	KMnO4	KMnO4/H2SO4	"
	3/4/98	HCl	25 ml HCl in DI	
1-O-M101A-3	3/4/98	KMnO4	KMnO4/H2SO4	"
	3/4/98	HCl	25 ml HCl in DI	
2-O-M101A-FB	3/4/98	KMnO4	KMnO4/H2SO4	"
	3/4/98	HCl	25 ml HCl in DI	

leaky KMNO4

leaky KMNO4 (SAVED)

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: Shawn Graham Date/Time: 3/4/98

Transported by: FedEx Date/Time: 3/4/98

Transported to: Philip Analytical Services
299 Cayuga Rd.
Cheekpowaga, NY 14225

Received by: Ancy Sebastian Date/Time: 98/03/05 1:30 pm

EMISSIONS CHARACTERIZATION AND TESTING SERVICES

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 665-SG JOB NAME: Ogden - Lake

LABORATORY: Phillip JOB No.: 10382

DATE SAMPLES WERE TRANSMITTED: 3-Mar-98 EXPECTED DATE OF RESULTS: 6-Mar-98

SAMPLE MATRIX: 4% KMnO4/10% H2SO4

TYPE OF ANALYSIS REQUIRED: Please analyze according to EPA Method 101A for Hg only.

101A

Sample / Run ID #	Sample Collection Date	Sample Components	Sample Matrix	Condition of Samples
2-I-M101A-3 ✓	3/3/98	KMnO4	KMnO4/H2SO4	(w/filter) 1L, 500c/d
	3/3/98	HCl	25 ml HCl in DI	
2-I-M101A-β) 4	3/3/98	KMnO4	KMnO4/H2SO4	(w/filter)
on the bottle	3/3/98	HCl	25 ml HCl in DI	
2-O-M101A-α) 3	3/3/98	KMnO4	KMnO4/H2SO4	
on the bottle	3/3/98	HCl	25 ml HCl in DI	
2-O-M101A-4	3/3/98	KMnO4	KMnO4/H2SO4	
	3/3/98	HCl	25 ml HCl in DI	
Reagent Blank	3/3/98	KMnO4	KMnO4/H2SO4	leaked out ≈ 25m
		HCl	25 ml HCl in DI	

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: Shawn Graham Date/Time: 3/3/98

Transported by: FedEx Date/Time: 3/3/98

Transported to: Philip Analytical Services
299 Cayuga Rd.
Cheekpowaga, NY 14225

Received by: Ancy Sebastian Date/Time: 98103104 11:30 AM

SAMPLE LOG IN SHEET

Lab Name: Philip Analytical Services Corporation, Burlington Laboratory	
Received by (Print Name): ANCY SEBASTIAN	
Received by (Signature): <i>Ancy</i>	
Client Project ID: AIR KINETICS	
REMARKS	Condition of Samples/Sample Shipment:
Custody Seal(s) Present/Absent <u>Present</u>	
Chain of Custody Records Present/Absent <u>Present</u>	
Airbill Present/Absent <u>Present</u>	
Airbill No: 801042153457 928706005	
Does Information on Custody Records and Samples Agree? Yes/No <u>Yes</u>	→ KMNDy leaked out from 1-1-R3 and F.B.
Date Received at Lab 3-5-98	
Time Received 130	
Temperature of Coolers	
Cooler ID:	Temperature
2 Boxes	

Relinquished By: RT
Date: _____

Logbook No: _____
Logbook Page No: _____

SAMPLE LOG IN SHEET

AIRKINETICS

Lab Name: Philip Analytical Services Corporation, Burligton Laboratory				
Received by (Print Name): ANCY SEBASTIAN				
Received by (Signature): <i>Ancy</i>				
Client Project ID: AIR KEN				
REMARKS	Condition of Samples/Sample Shipment:			
Custody Seal(s) Present/Absent <u>Present</u>				
Chain of Custody Records <u>Present</u> /Absent				
Airbill <u>Present</u> /Absent				
Airbill No: 801042153468				
<table border="1" style="margin: auto;"> <tr> <td style="padding: 2px;">928</td> <td style="padding: 2px;">7706</td> <td style="padding: 2px;">057</td> </tr> </table> <p style="font-size: small; margin: 0;">PACKING NUMBER — PULL UP PURPLE TAB</p>	928	7706	057	
928	7706	057		
Does Information on Custody Records and Samples Agree? Yes <u>No</u>	1p's on the c of c was wrong for 2 samples & some km04 leak out			
Date Received at Lab 09 04 98				
Time Received 1130				
Temperature of Coolers				
Cooler ID:	Temperature			
2 Box coolers	12° 14°			

Relinquished By: _____

Date: _____

Logbook No: _____


Logbook Page No: _____

FedEx USA Airbill

FedEx Tracking Number **801042153457**

0200 Form I.D. No.

Recipient's Copy

1 From 

Date **3/4/98**

Sender's Name **SHAWN GRAHAM** Phone **135213651611**

Company **AIRKINETICS (C/O OGDEN MARTIN OF LAKE)**

Address **3830 ROGERS INDUSTRIAL PARK** Dept./Floor/Suite/Room

City **OKAHUMPKA** State **FL** ZIP **34762**

2 Your Internal Billing Reference Information

3 To Recipient's Name **ROO McLOUG** Phone **190513328788**

Company **PHILIP ANALYTICAL SERVICES**

Address **299 CAYUGA RD** Dept./Floor/Suite/Room
(To "HOLD" at FedEx location, print FedEx address here)

City **CHEEKPOWAGA** State **NY** ZIP **14225**

For HOLD at FedEx Location check here
 Hold Weekday (Not available with FedEx First Overnight)
 Hold Saturday (Not available at all locations) (Available for FedEx Priority Overnight and FedEx 2Day only)

For Saturday Delivery check here
 (Extra Charge. Not available to all log skids) (Available for FedEx Priority Overnight and FedEx 2Day only)

Check here if residence (Extra charge applies for FedEx Express Saver)



4a Express Package Service Packages under 150 lbs. Delivery commitment may be later in some areas.

FedEx Priority Overnight (Next business morning) FedEx Standard Overnight (Next business afternoon) FedEx 2Day* (Second business day) FedEx Express Saver* (Third business day)

FedEx First Overnight (Earliest next business morning delivery to select locations) (Higher rates apply) * FedEx Letter Rate not available. Minimum charge: One pound rate.

4b Express Freight Service Packages over 150 lbs. Delivery commitment may be later in some areas.

FedEx Overnight Freight (Next business day) FedEx 2Day Freight (Second business day) FedEx Express Saver Freight (Up to 3 business days)

(Call for delivery schedule. See back for detailed descriptions of freight services.)

5 Packaging FedEx Letter FedEx Pak FedEx Box FedEx Tube Other Pkg. Declared value limit \$500.

6 Special Handling Does this shipment contain dangerous goods? Yes (As per attached Shipper's Declaration) Yes (Shipper's Declaration not required) No

Dry Ice (Dry Ice, 9 UN 1845 III, _____ x _____ kg, 904 (Dangerous Goods Shipper's Declaration not required)) CA Cargo Aircraft Only

7 Payment Obtain Recipient FedEx Account No.

Bill to: Sender (Account no. in which bill will be billed) Recipient (Enter FedEx account no. or Credit Card no. below) Third Party Credit Card Cash/Check



Total Packages **2** Total Weight **55** Total Declared Value \$ **.00** Total Charges \$

*When declaring a value higher than \$100 per shipment, you pay an additional charge. See SERVICE CONDITIONS, DECLARED VALUE, AND LIMIT OF LIABILITY section for further information. Credit Card Auth.

8 Release Signature

Your signature authorizes Federal Express to deliver this shipment without obtaining a signature and agrees to indemnify and hold harmless Federal Express from any resulting claims.

Questions? Call 1-800-Go-FedEx (800)463-3339

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000051

FedEx USA-Airbill

FedEx Tracking Number **801042153468**

0200 Form I.D. No.

Recipient's Copy

1 From
Date 3/3/98

Sender's Name SHAWN GRAHAM Phone (352) 365 1611

Company AIRKINETICS (C/O LAKECO. RRF)

Address 3830 ROGERS INDUSTRIAL PARK Dept./Floor/Suite/Room

City OKAHUMPKA State FL ZIP 34762

2 Your Internal Billing Reference Information 10382

3 To
Recipient's Name ROO McLOUS Phone (905) 332 8788

Company Philip Analytical Services

Address 299 CAYUGA RD Dept./Floor/Suite/Room

City Chicksonaga State NY ZIP 14225

For HOLD at FedEx Location check here
 Hold Weekday (Not available with FedEx First Overnight)
 Hold Saturday (Not available at all locations) (Available for FedEx Priority Overnight and FedEx 2Day only)

For Saturday Delivery check here
 (Extra Charge. Not available at all locations) (Available for FedEx Priority Overnight and FedEx 2Day only)



4a Express Package Service Packages under 150 lbs. Delivery commitment may be later in some areas.
 FedEx Priority Overnight (Next business morning) FedEx Standard Overnight (Next business afternoon) FedEx 2Day* (Second business day)
 FedEx Express Saver* (Third business day)

FedEx First Overnight (Earliest next business morning delivery to select locations) (Higher rates apply) * FedEx Letter Rate not available. Minimum charge: One pound rate.

4b Express Freight Service Packages over 150 lbs. Delivery commitment may be later in some areas.
 FedEx Overnight Freight (Next business day) FedEx 2Day Freight (Second business day) FedEx Express Saver Freight (Up to 3 business days)
(Call for delivery schedule. See back for detailed descriptions of freight services.)

5 Packaging FedEx Letter (Declared value limit \$500) FedEx Pak FedEx Box FedEx Tube Other Pkg.

6 Special Handling
Does this shipment contain dangerous goods? Yes (As per attached Shipper's Declaration) Yes (Shipper's Declaration not required)
 Dry Ice (Dry Ice, UN 1845 III, _____ x _____ kg, 904 (Dangerous Goods Shipper's Declaration not required)) Cargo Aircraft Only

7 Payment
Bill to: Sender (Account no. in section 7 will be billed) Recipient (Enter FedEx account no. or Credit Card no. below) Third Party Credit Card Cash/Check Obtain Recipient FedEx Account No.



Total Packages 2 Total Weight 111 Total Declared Value* \$.00 Total Charged \$ _____
*When declaring a value higher than \$100 per shipment, you pay an additional charge. See SERVICE CONDITIONS, DECLARED VALUE, AND LIMIT OF LIABILITY section for further information. Credit Card Auth.

8 Release Signature

Your signature authorizes Federal Express to deliver this shipment without obtaining a signature and agrees to indemnify and hold harmless Federal Express from any resulting claims.

Questions? **287**
Call 1-800-Go-FedEx (800)463-3339
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D 84

000052

NOTICE OF SAMPLE RECEIPT-ZENON LABORATORIES

000053

Attention: Shawn Graham
 Client: AirKineticd, Inc.
 Re Client Project: 10382
 FAX #: 714 895 1915
 Phone #: 714 373 0998

Samples for: Hg via 101A
 were received in good condition unless
 indicated below.

SAMPLE LISTING

Zenon ID #	Sample ID	Date Sampled	Date Received
-----	-----	-----	-----
009541	1-I-M101A-2	98/03/04	98/03/05
009542	1-I-M101A-3	98/03/04	98/03/05
009543	1-O-M101A-2	98/03/04	98/03/05
009544	1-O-M101A-3	98/03/04	98/03/05
009545	2-O-M101A-FB	98/03/04	98/03/05

Comments: Minor leakage from the FB
VMODU again. We will analyze only
the sample remaining in the bottle

Date 98/03/06

Roy D 85

NOTICE OF SAMPLE RECEIPT-ZENON LABORATORIES

000054

Attention: Shawn Graham
 Client: AirKineticd, Inc.
 Re Client Project: 10382
 FAX #: 714 895 1915
 Phone #: 714 373 0998

Samples for: 101A Hg.
 were received in good condition unless
 indicated below.

SAMPLE LISTING

Zenon ID #	Sample ID	Date Sampled	Date Received
-----	-----	-----	-----
009246	2-I-M101A-3	98/03/03	98/03/04
009247	2-I-M101A-4	98/03/03	98/03/04
009248	2-O-M101A-3	98/03/03	98/03/04
009249	2-O-M101A-4	98/03/03	98/03/04
009250	Reagent Blank	98/03/03	98/03/04

Comments: ① Samples logged as per bottle
ID#, not C-of-C ID

② Reagent Bix lost ~25 ml into the plastic bag. D 86

Date 98/03/05 We will analyze from remaining
 KMnO₄/H₂SO₄ within the bottle. Rm

**5. INTERNAL LAB SAMPLE TRANSFER RECORDS AND
TRACKING SHEET**

- Describe or list

6. OTHER RECORDS

- Telephone Communication Log

- Other



**DATA PACKAGE
FOR
AIR KINETICS Inc.
*Project # 10382
OMS: LAKE***

**Philip Analytical Services
5555 North Service Road
Burlington, ON L7L 5H7**

Submission #: 8C0242, 8C0254 & 8C0251

Prepared by : Colin McGandy - CSR
Approved by : Dr. Ron McLeod - Principal Scientist

Initial : CM
Initial : RM



000001

1.0 PROJECT NARRATIVE

PROJECT NARRATIVE

PHILIP Analytical Services (Burlington ON)

Philip Project: AN980186

Philip Submission #:8C0242

Client: Air Kinetics, Inc.

Client Project: 10382

I. SAMPLE RECEIPT/ANALYSIS

a) Sample Listing

Philip ID	Client Sample ID	Date Sampled	Date Received	Date Prepped	Run Date
<i>Mercury 1B via CVAA</i>					
010220 98	Method Blank	98/03/04	98/03/10	98/03/11	98/03/12
010227 98	2-O-MM101A-1	98/03/03	98/03/10	98/03/11	98/03/12
010228 98	1-I-MM101A-1	98/03/04	98/03/10	98/03/11	98/03/12
010229 98	2-I-MM101A-1	98/03/03	98/03/10	98/03/11	98/03/12
<i>Mercury 3B via CVAA</i>					
010220 98	Method Blank	98/03/04	98/03/10	98/03/10	98/03/11
010226 98	1-O-MM101A-1	98/03/04	98/03/10	98/03/10	98/03/11
010227 98	2-O-MM101A-1	98/03/03	98/03/10	98/03/10	98/03/11
010228 98	1-I-MM101A-1	98/03/04	98/03/10	98/03/10	98/03/11
010229 98	2-I-MM101A-1	98/03/03	98/03/10	98/03/10	98/03/11
<i>Mercury 3C via CVAA</i>					
010220 98	Method Blank	98/03/04	98/03/10	98/03/11	98/03/13
010226 98	1-O-MM101A-1	98/03/04	98/03/10	98/03/11	98/03/13
010227 98	2-O-MM101A-1	98/03/03	98/03/10	98/03/11	98/03/13
010228 98	1-I-MM101A-1	98/03/04	98/03/10	98/03/11	98/03/13
010229 98	2-I-MM101A-1	98/03/03	98/03/10	98/03/11	98/03/13
<i>Mercury via SW846 Method 7471</i>					
010231 98	Carbon Sample	98/03/04	98/03/10	98/03/12	98/03/13

Mercury via CVAA

010220 98	Method Blank	98/03/04	98/03/10	98/03/11	98/03/12
010221 98	1-O-MM101A-1 KCI1,2	98/03/04	98/03/10	98/03/11	98/03/12
010222 98	2-O-MM101A-1 KCI1,2	98/03/03	98/03/10	98/03/11	98/03/12
010223 98	1-I-MM101A-1 KCI1,2	98/03/04	98/03/10	98/03/11	98/03/12
010224 98	2-I-MM101A-1 KCI1,2	98/03/03	98/03/10	98/03/11	98/03/12
010225 98	MM101A-RB 11,2	98/03/09	98/03/10	98/03/11	98/03/12
010307 98	1-O-MM101A-1 KCI3	98/03/04	98/03/10	98/03/11	98/03/12
010308 98	2-O-MM101A-1 KCI3	98/03/03	98/03/10	98/03/11	98/03/12
010309 98	1-I-MM101A-1 KCI3	98/03/04	98/03/10	98/03/11	98/03/12
010310 98	2-I-MM101A-1 KCI3	98/03/03	98/03/10	98/03/11	98/03/12
010311 98	MM101A-RB I3	98/03/09	98/03/10	98/03/11	98/03/12
010353 98	1-O-IMP1/2 split	98/03/04	98/03/10	98/03/11	98/03/13
010354 98	2-O-IMP1/2 split	98/03/04	98/03/10	98/03/11	98/03/12
010355 98	2-O-IMP3 split	98/03/04	98/03/10	98/03/11	98/03/12
010356 98	1-I-IMP1/2 split	98/03/04	98/03/10	98/03/11	98/03/12
010357 98	2-I-IMP1/2 split	98/03/04	98/03/10	98/03/11	98/03/12
010358 98	2-I-IMP3 split	98/03/04	98/03/10	98/03/11	98/03/12

Run Date is defined as the date of injection of the last calibration standard (12 hour or less) prior to the samples analyzed within that run sequence. Therefore the time of calibration injection that defines the run date is always within 12 hours of the time of sample injection.

- b) Shipping Problems: none encountered
 c) Documentation Problems: none encountered

II. SAMPLE PREP:

No problems encountered


III. SAMPLE ANALYSIS:

See also comments within the appropriate Certificate of Analysis.

- a) Hold Times: all within recommended hold times
 b) Instrument Calibration: all within control limits

I certify that this data package is in compliance with the terms and conditions of the contract, both technically and for completeness, for other than the conditions detailed above.

In addition, I certify, that to the best of my knowledge and belief, the data as reported are true and accurate. Release of the data contained in this data package has been authorized by the cognizant laboratory official or his/her designee, as verified by this signature.


 Ronald A. McLeod, Principal Sci. Ph.D., C.Chem.

980322
 Date

2.0 CERTIFICATE OF ANALYSIS

Certificate of Analysis

CLIENT INFORMATION

Attention: Shawn Graham
Client Name: Air Kinetics, Inc.
Project: 10382
Project Desc: OMS - Lake
Address: 5932 Bolsa Avenue, Suite 105
Huntington Beach, CA
CA 92649
Fax Number: 714 895 1915
Phone Number: 714 373 0998

LABORATORY INFORMATION

Contact: Ron McLeod
Project: AN980186
Date Received: 98/03/10
Date Reported: 98/03/13
Submission No.: 8C0242
Sample No.: 010220-010358

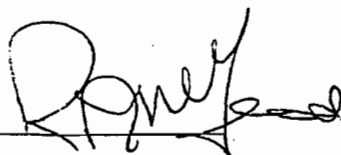
NOTES: *"-" = not analysed '<' = less than Method Detection Limit (MDL) 'NA' = no data available*
LOQ can be determined for all analytes by multiplying the appropriate MDL X 3.33
Solids data is based on dry weight except for biota analyses.
Organic analyses are not corrected for extraction recovery standards except for isotope dilution methods, (i.e. CARB 429 PAH, all PCDD/F and DBD/DBF analyses)

Methods used by PASC are based upon those found in 'Standard Methods for the Examination of Water and Wastewater', Seventeenth Edition. Other methods are based on the principles of MISA or EPA methodologies. New York State: ELAP Identification Number 10756.

All work recorded herein has been done in accordance with normal professional standards using accepted testing methodologies, quality assurance and quality control procedures except where otherwise agreed to by the client and testing company in writing. Any and all use of these test results shall be limited to the actual cost of the pertinent analysis done. There is no other warranty expressed or implied. Your samples will be retained at PASC for a period of three weeks from receipt of data or as per contract.

COMMENTS:

Certified by:



Page 1

PASC - Certificate of Analysis

Component	MDL	Units	Method	Blank	% Recovery	Blank Spike	% Recovery	1-O-MM101A-1	1-O-MM101A-1
			Blank	Spike		Duplicate		KCII,2	KCII,2
			010220 98	010220 98	010220 98	010220 98	010220 98	010221 98	010221 98
			98/03/04	98/03/04	98/03/04	98/03/04	98/03/04	98/03/04	98/03/04
									Duplicate
Impinger volume measured		"	100	-	-	-	-	240	-
Mercury - FH	0.030	ug	<	0.33	110	0.32	110	-	-
Mercury - KMNO4	0.050	"	<0.10	1.1	110	1.1	110	-	-
Mercury - HCl digestate	0.050	"	<	0.53	110	0.53	110	-	-
Mercury	0.010	"	<	0.11	110	0.11	110	32	31

D 95

000006

PASC - Certificate of Analysis

Component	MDL	Units	1-O-MM101A-1	1-O-MM101A-1	1-O-MM101A-1	1-O-MM101A-1	2-O-MM101A-1	1-I-MM101A-1
			Client ID: KCII,2	Client ID: KCII,2	Client ID: KCII,2	Client ID: KCII,2	Client ID: KCII,2	Client ID: KCII,2
			010221 98	010221 98	010221 98	010221 98	010222 98	010223 98
			98/03/04	98/03/04	98/03/04	98/03/04	98/03/03	98/03/04
			M. Spike	MS % Rec.	MS Dup	MSD % Rec.		
Impinger volume measured		"	-	-	-	-	250	220
Mercury - FH	0.030	ug	-	-	-	-	-	-
Mercury - KMNO4	0.050	"	-	-	-	-	-	-
Mercury - HCl digestate	0.050	"	-	-	-	-	-	-
Mercury	0.010	"	55	99	54	95	3.3	56

96 0

000007

PASC - Certificate of Analysis

Component	MDL	Units	2-I-MM101A-1	MM101A-RB	1	1	1	1
			Client ID: KCI1,2	I1,2	O-MM101A-1	O-MM101A-1	O-MM101A-1	O-MM101A-1
			010224 98	010225 98	010226 98	010226 98	010226 98	010226 98
			98/03/03	98/03/09	98/03/04	98/03/04	98/03/04	98/03/04
					Duplicate	M. Spike	MS % Rec.	
Impinger volume measured		"	170	200	-	-	-	-
Mercury - FH	0.030	ug	-	-	-	-	-	-
Mercury - KMNO4	0.050	"	-	-	<0.10	<0.10	1.1	110
Mercury - HCl digestate	0.050	"	-	-	0.16	0.15	0.70	110
Mercury	0.010	"	27	<0.020	-	-	-	-

D 97

800000

PASC - Certificate of Analysis

Component	MDL	Units	1	1	2	2	2	2	2
			MS Dup	MSD % Rec.	Duplicate	M. Spike	MS % Rec.	MS Dup	
Impinger volume measured		"	-	-	-	-	-	-	-
Mercury - FH	0.030	ug	-	-	0.48	0.49	0.77	96	0.81
Mercury - KMNO4	0.050	"	1.1	110	<0.10	-	-	-	-
Mercury - HCl digestate	0.050	"	0.69	110	0.062	-	-	-	-
Mercury	0.010	"	-	-	-	-	-	-	-

Client ID:

Lab No.:

Date Sampled:

O-MM101A-1 O-MM101A-1 O-MM101A-1 O-MM101A-1 O-MM101A-1 O-MM101A-1 O-MM101A-1 O-MM101A-1

010226 98 010226 98 010227 98 010227 98 010227 98 010227 98 010227 98 010227 98

98/03/04 98/03/04 98/03/03 98/03/03 98/03/03 98/03/03 98/03/03 98/03/03

86 0

000009

PASC - Certificate of Analysis

Component	MDL	Units	2	1	2	1-O-MM101A-1	2-O-MM101A-1	1-I-MM101A-1
			O-MM101A-1	I-MM101A-1	I-MM101A-1	KCII3	KCII3	KCII3
<i>Client ID:</i>			O-MM101A-1	I-MM101A-1	I-MM101A-1	KCII3	KCII3	KCII3
<i>Lab No.:</i>			010227 98	010228 98	010229 98	010307 98	010308 98	010309 98
<i>Date Sampled:</i>			98/03/03	98/03/04	98/03/03	98/03/04	98/03/03	98/03/04
		MSD % Rec.						
Impinger volume measured		"	-	-	-	160	80	150
Mercury - FH	0.030	ug	110	70	32	-	-	-
Mercury - KMNO4	0.050	"	-	<0.10	0.17	-	-	-
Mercury - HCl digestate	0.050	"	-	3.9	1.9	-	-	-
Mercury	0.010	"	-	-	-	0.80	<	0.95

PASC - Certificate of Analysis

Component	MDL	Units	2-I-MM101A-1	MM101A-RB	1-O-IMP1/2	1-O-IMP1/2	1-O-IMP1/2	1-O-IMP1/2	1-O-IMP1/2
			Client ID: KCIH3	I3	split	split	split	split	split
			010310 98	010311 98	010353 98	010353 98	010353 98	010353 98	010353 98
			98/03/03	98/03/09	98/03/04	98/03/04	98/03/04	98/03/04	98/03/04
					Duplicate	M. Spike	MS % Rec.	MS Dup	
Impinger volume measured		"	90	100	220	-	-	-	-
Mercury - FH	0.030	ug	-	-	-	-	-	-	-
Mercury - KMNO4	0.050	"	-	-	-	-	-	-	-
Mercury - HCl digestate	0.050	"	-	-	-	-	-	-	-
Mercury	0.010	"	0.017	<	33	33	74	96	72

D100

000011

PASC - Certificate of Analysis

<i>Client ID:</i>	1-O-IMP1/2	2-O-IMP1/2	2-O-IMP3	1-I-IMP1/2	2-I-IMP1/2	2-I-IMP3
<i>Lab No.:</i>	split	split	split	split	split	split
<i>Date Sampled:</i>	010353 98	010354 98	010355 98	010356 98	010357 98	010358 98
	98/03/04	98/03/04	98/03/04	98/03/04	98/03/04	98/03/04

Component	MDL	Units	MSD % Rec.					
Impinger volume measured		"	-	210	85	220	210	80
Mercury - FH	0.030	ug	-	-	-	-	-	-
Mercury - KMNO4	0.050	"	-	-	-	-	-	-
Mercury - HCl digestate	0.050	"	-	-	-	-	-	-
Mercury	0.010	"	91	3.4	0.056	69	36	0.22

D101

000019

Batch Code: 0311ASA3
 Mercury 010220 98
 010227 98
 010228 98
 010229 98
 Date analysed 98/03/12
 Date prepared 98/03/11

Batch Code:	0311ASA1	0311ASA2	0311ASA2
Mercury	010220 98	010353 98	010354 98
	010221 98		010355 98
	010222 98		010356 98
	010223 98		010357 98
	010224 98		010358 98
	010225 98		
	010307 98		
	010308 98		
	010309 98		
	010310 98		
	010311 98		
Date analysed	98/03/12	98/03/13	98/03/12
Date prepared	98/03/11	98/03/11	98/03/11



Certificate of Analysis

CLIENT INFORMATION

Attention: Shawn Graham
Client Name: Air Kinetics, Inc.
Project: 10382
Project Desc: OMS - Lake
Address: 5932 Bolsa Avenue, Suite 105
 Huntington Beach, CA
 CA 92649
Fax Number: 714 895 1915
Phone Number: 714 373 0998

LABORATORY INFORMATION

Contact: Ron McLeod
Project: AN980186
Date Received: 98/03/10
Date Reported: 98/03/13
Submission No.: 8C0242
Sample No.: 010230-010231

NOTES:

'-' = not analysed '<' = less than Method Detection Limit (MDL) 'NA' = no data available
 LOQ can be determined for all analytes by multiplying the appropriate MDL X 3.33
 Solids data is based on dry weight except for biota analyses.
 Organic analyses are not corrected for extraction recovery standards except for isotope
 dilution methods, (i.e. CARB 429 PAH, all PCDD/F and DBD/DBF analyses)

Methods used by PASC are based upon those found in 'Standard Methods for the Examination of Water and Wastewater', Seventeenth Edition. Other methods are based on the principles of MISA or EPA methodologies. New York State: ELAP Identification Number 10756.

All work recorded herein has been done in accordance with normal professional standards using accepted testing methodologies, quality assurance and quality control procedures except where otherwise agreed to by the client and testing company in writing. Any and all use of these test results shall be limited to the actual cost of the pertinent analysis done. There is no other warranty expressed or implied. Your samples will be retained at PASC for a period of three weeks from receipt of data or as per contract.

COMMENTS:

Sample was analysed 98/03/12

Certified by:

PASC - Certificate of Analysis

	Method	Blank	% Recovery	Carbon		
	Blank	Spike		Sample		
<i>Client ID:</i>						
<i>Lab No.:</i>	010230 98	010230 98	010230 98	010231 98		
<i>Date Sampled:</i>	98/03/04	98/03/04	98/03/04	98/03/04		
Component	MDL	Units				
Mercury via SW846 Method 7471	0.04	mg/kg	<	0.96	96	<

D104

000015

5.0 SHIPPING/RECEIVING DOCUMENTS

Airbills (No. of shipments = _____)

Chain-of-Custody Records

Sample Log-In Sheets

Miscellaneous Shipping/Receiving Records (describe or list)

Lab Name: Philip Analytical Services Corporation, Burlington Laboratory

Received by (Print Name): K. Caruana

Received by (Signature): [Signature]

Client Project ID: AIRKINETICS

REMARKS

Condition of Samples/Sample Shipment:

Custody Seal(s)

Present/Absent

Samples rec'd intact

Chain of Custody Records

Present/Absent

Airbill

Present/Absent

Airbill No:

357 2435 072

357 7431 496

357 2435 246

351 8831 014

Does Information on Custody Records and Samples Agree?

Yes/No

Date Received at Lab

3-10-98

Time Received

1:40 pm.

Temperature of Coolers

Cooler ID:

Temperature

4 CASES

not taken

Relinquished By: RT

Logbook No: _____

Date: 9/30/30

Logbook Page No: _____

AirKinetics, Inc.

EMISSIONS CHARACTERIZATION AND TESTING SERVICES

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 667 - GM JOB NAME: OMS - Lake

LABORATORY: Philip Analytical Services JOB No.: 10382

DATE SAMPLES WERE TRANSMITTED: 9-Mar-98 EXPECTED DATE OF RESULTS: 13-Mar-98

SAMPLE MATRIX: 0.1M KCl, 4% KMnO4/10% H2SO4, 8N HCl and 0.1N HNO3

TYPE OF ANALYSIS REQUIRED: Please analyze each fraction separately for mercury (Hg). Analyze the KMnO4 and 8N HCl Rinse according to EPA Method 101A. Analyze carbon sample for mercury (Hg).

Please Note - results are requested by Friday March 13, 1998.

MB-10220

10221
10227

10224

10231

Sample (Run ID)	Sample Collection Date	Sample Components	Sample Matrix	Condition of Sample
1-O-MM101A-1	03/04/98	1st & 2nd Imp. ✓	0.1M KCl	ILP Mercur
		3rd Imp. ✓	0.1M KCl	500g
		KMnO4 ✓	KMnO4/H2SO4	1LCC
		8N HCl Rinse ✓	8N HCl	500g } M29HG
		Imp. 1 & 2 split sample w/KMnO4 ✓	KMnO4/H2SO4	500g }
Carbon Sample		Carbon	Carbon	plastic bag

UBS-10230

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: *[Signature]* Date/Time: 3/9/98 1430

Transported by: FedEx Date/Time: 3/9/98

Transported to: Philip Analytical Services
5555 North Service Road
Burlington, Ontario Canada L7L 5H7

Received by: *[Signature]* Date/Time: 980310 140p

EMISSIONS CHARACTERIZATION AND TESTING SERVICE

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 667 - GM

JOB NAME: OMS - Lake

LABORATORY: Philip Analytical Services

JOB No.: 10382

DATE SAMPLES WERE TRANSMITTED: 9-Mar-98

EXPECTED DATE OF RESULTS: 13-Mar-98

SAMPLE MATRIX: 0.1M KCl, 4% KMnO4/10% H2SO4, 8N HCl and 0.1N HNO3

TYPE OF ANALYSIS REQUIRED: Please analyze each fraction separately for mercury (Hg). Combine F1/2 0.1N HNO3 Rinse with 1st & 2nd Impinger for a single fraction. Analyze the KMnO4 and 8N HCl Rinse according to EPA Method 101A. Please Note - results are requested by Friday March 13, 1998.

Sample Run ID	Sample Collection Date	Sample Components	Sample Matrix	Condition of Sample
10222 10305	03/03/98	1st & 2nd Imp. ✓	0.1M KCl	W/P
		3rd Imp. ✓	0.1M KCl	SOCG
		KMnO4 ✓	KMnO4/H2SO4	W/P
		8N HCl Rinse ✓	8N HCl	SOCG
		F1/2 0.1N HNO3 rinse ✓	0.1N HNO3	SOCG
		Imp. 1 & 2 split sample w/KMnO4 ✓	KMnO4/H2SO4	W/P
		Imp. 3 split sample w/ KMnO4 ✓	KMnO4/H2SO4	SOCG

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: [Signature]

Date/Time: 3/9/98 1430

Transported by: FedEx

Date/Time: 3/9/98

Transported to: Philip Analytical Services
5555 North Service Road
Burlington, Ontario Canada L7L 5H7

D108

Received by: [Signature]

Date/Time: 980310 1:40

EMISSIONS CHARACTERIZATION AND TESTING SERVICE

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 667 - GM

JOB NAME: OMS - Lake

LABORATORY: Philip Analytical Services

JOB No.: 10382

DATE SAMPLES WERE TRANSMITTED: 9-Mar-98

EXPECTED DATE OF RESULTS: 13-Mar-98

SAMPLE MATRIX: 0.1M KCl, 4% KMnO4/10% H2SO4, 8N HCl and 0.1N HNO3

TYPE OF ANALYSIS REQUIRED: Please analyze each fraction separately for mercury (Hg). Analyze the KMnO4 and 8N HCl Rinse according to EPA Method 101A. Please Note - results are requested by Friday March 13, 1998.

10224
10230
10229
10225
10311

Sample/Run ID	Sample Collection Date	Sample Components	Sample Matrix	Condition of Samples
2-I-MM101A-1	03/03/98	1st & 2nd Imp. ✓	0.1M KCl	1LP
		3rd Imp. ✓	0.1M KCl	500P
		KMnO4 ✓	KMnO4/H2SO4	1LP
		8N HCl Rinse ✓	8N HCl	500P
		1/2 0.1N HNO3 rinse ✓	0.1N HNO3	500P
	10257	Imp. 1 & 2 split sample w/KMnO4	KMnO4/H2SO4	1LP
		Imp. 3 split sample w/KMnO4 ✓	KMnO4/H2SO4	500P
MM101A - RB	03/09/98	1st & 2nd Imp.	0.1M KCl	1LP
		0.1N HNO3	0.1N HNO3	500P

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: Mary M. J.

Date/Time: 3/9/98 1430

Transported by: FedEx

Date/Time: 3/9/98

Transported to: Philip Analytical Services
5555 North Service Road
Burlington, Ontario Canada L7L 5H7

Received by: [Signature]

Date/Time: 3/9/98 1:40

EMISSIONS CHARACTERIZATION AND TESTING SERVICES

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 667 - GM JOB NAME: OMS - Lake

LABORATORY: Philip Analytical Services JOB No.: 10382

DATE SAMPLES WERE TRANSMITTED: 9-Mar-98 EXPECTED DATE OF RESULTS: 13-Mar-98

SAMPLE MATRIX: 0.1M KCl, 4% KMnO4/10% H2SO4, 8N HCl and 0.1N HNO3

TYPE OF ANALYSIS REQUIRED: Please analyze each fraction separately for mercury (Hg). Analyze the KMnO4 and 8N HCl Rinse according to EPA Method 101A. Please Note - results are requested by Friday March 13, 1998.

Sample / Run ID	Sample Collection Date	Sample Components	Sample Matrix	Condition of Sample
1-I-MM101A-1	03/04/98	1st & 2nd Imp ✓	0.1M KCl	ILP
		3rd Imp. ✓	0.1M KCl	50DP
		KMnO4 ✓	KMnO4/H2SO4	ILC
		8N HCl Rinse ✓	8N HCl	50DP
		F1/2 0.1N HNO3 rinse ✓	0.1N HNO3	50DP
	10/36	Imp. 1 & 2 split sample w/KMnO4 ✓	KMnO4/H2SO4	ILC

10223
10309
10228

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: [Signature] Date/Time: 3/9/98 1430

Transported by: FedEx Date/Time: 3/9/98

Transported to: Philip Analytical Services
5555 North Service Road
Burlington, Ontario Canada L7L 5H7

Received by: [Signature] Date/Time: 980310 1:40

D109

EMISSIONS CHARACTERIZATION AND TESTING SERVICES

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 667 - GM JOB NAME: OMS - Lake
 LABORATORY: Philip Analytical Services JOB No.: 10382
 DATE SAMPLES WERE TRANSMITTED: 9-Mar-98 EXPECTED DATE OF RESULTS: 13-Mar-98
 SAMPLE MATRIX: 0.1M KCl, 4% KMnO4/10% H2SO4, 8N HCl and 0.1N HNO3

TYPE OF ANALYSIS REQUIRED: Please analyze each fraction separately for mercury (Hg). Analyze the KMnO4 and 8N HCl Rinse according to EPA Method 101A. Please Note - results are requested by Friday March 13, 1998.

10223
10309
10228

Sample / Run ID	Sample Collection Date	Sample Components	Sample Matrix	Condition of Sample
1-I-MM101A-1	03/04/98	1st & 2nd Imp ✓	0.1M KCl	ILP
		3rd Imp. ✓	0.1M KCl	SDP
		KMnO4 ✓	KMnO4/H2SO4	ILP
		8N HCl Rinse ✓	8N HCl	SDP
		F1/2 0.1N HNO3 rinse ✓	0.1N HNO3	SDP
	10356	Imp. 1 & 2 split sample w/KMnO4 ✓	KMnO4/H2SO4	SDP

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: [Signature] Date/Time: 3/9/98 1430
 Transported by: FedEx Date/Time: 3/9/98
 Transported to: Philip Analytical Services
5555 North Service Road
Burlington, Ontario Canada L7L 5H7
 Received by: [Signature] Date/Time: 980310 1:40

D109

ENGINEERING TEST REPORT

UNIT NOS. 1 AND 2

Source Location:

Ogden Martin Systems of Lake, Inc.
3830 Rogers Industrial Park
Okahumpka, Florida 34762

Test Date: March 19 and 20, 1998
Issue Date: April 22, 1998
Revision: 0

Prepared for:

Ogden Energy Group, Inc.
40 Lane Road
Fairfield, New Jersey 07007

Prepared by:

AirKinetics, Inc.
AKI No.: 10388

Prepared By:

Sakhalin Finnie
Sakhalin Finnie
Report Coordinator

Reviewed By:

Sakhalin Finnie for
Shawn Graham
Project Manager



EMISSIONS CHARACTERIZATION
AND TESTING SERVICES

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1.0 SUMMARY

1.1 Source Information

Plant Name and Address: Ogden Martin Systems Of Lake, Inc.
3830 Rogers Industrial Park
Okahumpka, Florida 34762

Source Tested: Unit Nos. 1 and 2

Permit ID #: A035-193817

Plant Contact: Cecil Boatwright, Facility Manager

Phone Number: (352) 365-1611

1.2 Testing Firm Information

Firm Name and Address: AirKinetics, Inc.
5932 Bolsa Avenue, Suite 105
Huntington Beach, CA 92649

Firm Contact: Shawn Graham, Project Manager

Phone Number: (714) 373-0998 Ext. 27

Subcontractor: Quanterra Incorporated, West Sacramento, California

1.3 Test Information

Test Requested By: Ogden Energy Group, Inc.

Firm Contact: Joe Aldina, Sr. Vice President, Environmental Testing/CEM

Phone Number: (973) 882-4136

Test Objective: To determine oxidized and elemental mercury speciation, mercury emissions and control efficiency.

Test Methods:

EPA 1	Sampling Point Determination
EPA 2	Velocity and Flow Rate
EPA 3	Molecular Weight
EPA 4	Flue Gas Moisture Content
EPA 101A	Mercury
Mod. EPA 101A	Oxidized and Elemental Mercury
EPA 26	Hydrogen Chloride and Chlorine
ASTM D-5291	Carbon, Hydrogen, & Nitrogen in Ash
EPA 9038	Sulfates in Ash
SM 4500 CI-C	Chloride in Ash
EPA 340.2	Fluoride in Ash

Test Dates: March 19 and 20, 1998

1.4 Test Personnel

Test Coordinator: Joe Aldina, Ogden Energy Group, Inc.

AirKinetics Test Personnel:
Shawn Graham, Project Manager
Wayne Johnson, Team Leader
Alfred Gusman, Field Technician
Herbert Dixon, Laboratory Technician, TESTAR
David Brintle, Field Technician, TESTAR

2.0 TEST RESULTS AND DATA PRESENTATION

The results of the testing are summarized in Tables 2-1, 2-2, 2-3, and 2-4. Results tabulations are presented in Appendix A. Example calculations are given in Appendix B. Field data are given in Appendix C. Analytical data are provided in Appendix D.

**TABLE 2-1
 UNIT 1 MERCURY TEST RESULTS**

Parameter	Units	Run 1	Run 2	Run 4	Run 5	Run 6	Run 7
Unit No. 1 Inlet							
Mercury	ug/dscm @ 7% O ₂	87.4	799	192.4	81.9	1157	575
	lb/hr	0.00898	0.0844	0.0192	0.00862	0.119	0.0620
Unit No. 1 STACK							
Mercury	ug/dscm @ 7% O ₂	37.9	51.3	35.7	24.2	24.0	38.2
	lb/hr	0.00454	0.00578	0.00379	0.00267	0.00260	0.00407
	% Efficiency ^a	56.4	93.6	81.4	70.5	97.9	93.4

^a - Efficiency calculated using ug/dscm @ 7% O₂ results.

**TABLE 2-2
 UNIT 2 MERCURY TEST RESULTS**

Parameter	Units	Run 1	Run 2
Unit No. 2 INLET			
Mercury	ug/dscm @ 7% O ₂	145	202
	lb/hr	0.0136	0.0195
Unit No. 2 STACK			
Mercury	ug/dscm @ 7% O ₂	16.1	11.7
	lb/hr	0.00159	0.00118
	% Efficiency ^a	88.9	94.2

^a - Efficiency calculated using ug/dscm @ 7% O₂ results.

TABLE 2-3
UNIT 1 HYDROGEN CHLORIDE AND ASH TEST RESULTS

Parameter	Units	Run 1	Run 2
Hydrogen Chloride	ug	44,300	
Ash:			
Mercury	ppm	12.3	18.4
Selenium		< 2.0	< 2.0
Titanium		984	742
Vanadium		17	14
Calcium		168,000	162,000
Sulfate		9,600	9,500
Chloride		330,000	330,000
Fluoride		34.7	38.3
Carbon Content		% Wt.	1.28
Hydrogen Content	1.18		0.96
Nitrogen Content	< 0.05		< 0.05

TABLE 2-4
UNIT 1 HYDROGEN CHLORIDE AND CHLORINE TEST RESULTS

Parameter	Units	Results
Hydrogen Chloride	ug	44,300
Chlorine	ug	86,355
	ppmvd	58.0
	ppmvd @ 7% O ₂	84.8
O ₂	%	11.4

3.0 INTRODUCTION

On March 19 and 20, 1998 AirKinetics, Inc. conducted source emissions testing for Ogden Energy Group, Inc. at Ogden Martin Systems of Lake, Inc. in Okahumpka, Florida. The objective of the test program was to determine mercury and hydrogen chloride emissions. The testing was conducted on both Unit Nos. 1 and 2. The methods used during this test program were EPA Method 1 for sampling point determination, EPA Method 2 for velocity and flow rate, EPA Method 3 for molecular weight, EPA Method 4 for flue gas moisture content, EPA Method 5 for particulate, EPA Method 101A for mercury (Hg), EPA 26 for hydrogen chloride (HCl) and chlorine (Cl₂), ASTM D-5291 for carbon (C), hydrogen (H), and nitrogen (N) in ash samples, EPA 9038 for sulfates in ash samples, SM 4500 Cl-C for chloride (Cl) in ash, and EPA 340.2 for fluoride (F) in ash.

Following is a test log is presented in Table 3-1 which lists the test locations, sampling objectives, sampling methods, test dates, and run numbers for the test program.

**TABLE 3-1
 TEST LOG**

Sampling Objective	Sampling Method	Test Date	Run Numbers			
Unit No. 1 Inlet						
Hg Speciation	Mod. EPA 101A	3/19/98	1-I-MM101A-1	1-I-MM101A-2		
		3/20/98	1-I-MM101A-4	1-I-MM101A-5	1-I-MM101A-6	1-I-MM101A-7
Unit No. 1 Outlet						
Hg Speciation	Mod. EPA 101A	3/19/98	1-O-MM101A-1	1-O-MM101A-2		
		3/20/98	1-O-MM101A-4	1-O-MM101A-5	1-O-MM101A-6	1-O-MM101A-7
HCl & Cl ₂	EPA 26		1-O-M26-1			
Ash	Grab	3/19/98	Ash-1	Ash-2		
Unit No. 2 Inlet						
Hg	EPA 101A	3/18/98	2-I-M101-1			
Hg Speciation	Mod. EPA 101A		2-I-MM101A-1			
Unit No. 2 Outlet						
Hg	EPA 101A	3/18/98	2-O-M101-1			
Hg Speciation	Mod. EPA 101A		2-O-MM101A-1			

4.0 TEST CRITIQUE

No sampling train leaks were observed during testing. The average sampling rate for each test run was within 10% of isokinetic. A minimum sample volume of 30 standard cubic feet was collected.

A field blank was analyzed with 0.33 micrograms (ug) of Hg detected. A reagent blank was analyzed with no Hg detected. A method blank was performed with no Hg detected. A matrix spike and matrix duplicate were conducted with results within acceptable limits. All mercury analyses were performed in duplicate and the RPD's of the duplicate analyses were within the acceptable limits.

Test run 3 on Unit 1 was aborted due to an electrical storm. All of the EPA Method 101A test runs conducted on Unit 1 were modified to allow for speciation of the elemental and oxidized mercury. The train modification consisted of three extra impingers placed prior to the 10% H₂SO₄ / 4% KMnO₄ impingers. Each impinger contained approximately 100 ml of 0.1N KCl. These impingers were used to capture the oxidized Hg. The elemental Hg was then captured in the 10% H₂SO₄/4% KMnO₄ reagent.

APPENDIX A
RESULTS TABULATION

1.0 UNIT NO. 1

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA
 Test Location: UNIT No. 1

Run Number	Run Date	Operator
1-I-MM101A-1	03/19/98	ALFRED GUSMAN
1-O-MM101A-1	03/19/98	WAYNE JOHNSON

		<u>1-I-MM101A-1</u>	<u>1-O-MM101A-1</u>
	Run Start Time	1010	1010
	Run Stop Time	1123	1115
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.256	0.218
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	1.0138	0.9757
Pbar	Barometric Pressure, Inches Hg	29.6	29.6
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.55	1.38
Vm	Sampled Volume of Source Gas, Dry ACF	41.000	40.619
Vmm	Sampled Volume of Source Gas, Dry ACM	1.161	1.150
tm	Dry Gas Meter Temperature, Degrees F	74.3	86.3
Vmstd	Sampled Volume of Source Gas, Dry SCF	40.793	38.025
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.155	1.077
Vlc	Volume of Condensed Liquid, mL	148.3	181.3
Vwstd	Volume of Water Vapor, SCF	6.980	8.533
%H2O	Moisture Content, Percent by Volume	14.6	18.3
%H2Osat	Saturated Moisture Content, Percent by Volume	100	100
Mfd	Source Gas Dry Mole Fraction	0.854	0.817
%CO2	Source Gas CO2 Content, Percent by Dry Volume	8.4	8.7
%O2	Source Gas O2 Content, Percent by Dry Volume	11.3	10.8
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.8	29.8
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.1	27.7
Pg	Source Gas Static Pressure, Inches H2O	-2.50	-17.0
Ps	Source Gas Absolute Pressure, Inches Hg	29.4	28.4
ts	Source Gas Temperature, Degrees F	451.0	271.4
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.737	1.077
vs	Source Gas Velocity, Feet/Second	64.8	72.0
A	Source Cross Sectional Area, Square Inches	3,025	2,627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	39,719	44,013
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,125	1,246
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	81,631	78,783
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,312	2,231
%I	Average Isokinetic Sampling Rate, Percent	101	101
Fo	Fuel Factor	1.14	1.16

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>1-I-MM101A-1</u>	<u>1-Q-MM101A-1</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	69.7	29.7
ppmvd	Concentration, Parts per Million by Volume Dr	0.00724	0.00330
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.0105	0.00454
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.0103	0.00455
ug/DSCM	Concentration, Micrograms per DSCM	60.4	27.5
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	87.4	37.9
ug/DSCM@12%CO	Concentration, ug/DSCM @ 12% CO2	86.2	38.0
lb/hr	Emission Rate, Pounds per Hour	0.00898	0.00454
g/sec	Emission Rate, Grams Per Second	0.00113	0.000572

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA

Test Location: UNIT No. 1

Run Number	Run Date	Operator
1-J-MM101A-2	03/19/98	ALFRED GUSMAN
1-O-MM101A-2	03/19/98	WAYNE JOHNSON

		<u>1-J-MM101A-2</u>	<u>1-O-MM101A-2</u>
	Run Start Time	1355	1355
	Run Stop Time	1502	1459
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.256	0.216
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	1.0138	0.9757
Pbar	Barometric Pressure, Inches Hg	29.6	29.6
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.50	1.28
Vm	Sampled Volume of Source Gas, Dry ACF	41.520	39.100
Vmm	Sampled Volume of Source Gas, Dry ACM	1.176	1.107
tm	Dry Gas Meter Temperature, Degrees F	77.5	83.4
Vmstd	Sampled Volume of Source Gas, Dry SCF	41.056	36.791
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.163	1.042
Vlc	Volume of Condensed Liquid, mL	108.7	155.6
Vwstd	Volume of Water Vapor, SCF	5.116	7.323
%H2O	Moisture Content, Percent by Volume	11.1	16.6
%H2Osat	Saturated Moisture Content, Percent by Volume	100	100
Mfd	Source Gas Dry Mole Fraction	0.889	0.834
%CO2	Source Gas CO2 Content, Percent by Dry Volume	8.4	8.6
%O2	Source Gas O2 Content, Percent by Dry Volume	11.2	11.4
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.8	29.8
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.5	27.9
Pg	Source Gas Static Pressure, Inches H2O	-2.50	-17.0
Ps	Source Gas Absolute Pressure, Inches Hg	29.4	28.4
ts	Source Gas Temperature, Degrees F	449.3	267.9
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.715	1.034
vs	Source Gas Velocity, Feet/Second	63.2	70.1
A	Source Cross Sectional Area, Square Inches	3,025	2,627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	40,458	43,977
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,146	1,245
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	79,700	76,721
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,257	2,172
%I	Average Isokinetic Sampling Rate, Percent	99.4	100
Fo	Fuel Factor	1.15	1.10

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>1-I-MM101A-2</u>	<u>1-O-MM101A-2</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	647.9	36.6
ppmvd	Concentration, Parts per Million by Volume Dr	0.0668	0.00421
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.0958	0.00616
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.0955	0.00587
ug/DSCM	Concentration, Micrograms per DSCM	557	35.1
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	799	51.3
ug/DSCM@12%CO	Concentration, ug/DSCM @ 12% CO2	796	49.0
lb/hr	Emission Rate, Pounds per Hour	0.0844	0.00578
g/sec	Emission Rate, Grams Per Second	0.0106	0.000728

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA

Test Location: UNIT No. 1

Run Number	Run Date	Operator
1-I-MM101A-4	3/20/98	ALFRED GUSMAN
1-O-MM101A-4	3/20/98	WAYNE JOHNSON

		1-I-MM101A-4	1-O-MM101A-4
	Run Start Time	833	833
	Run Stop Time	943	936
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.256	0.218
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	1.0138	0.9757
Pbar	Barometric Pressure, Inches Hg	29.5	29.5
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.46	1.25
Vm	Sampled Volume of Source Gas, Dry ACF	40.709	38.610
Vmm	Sampled Volume of Source Gas, Dry ACM	1.153	1.093
tm	Dry Gas Meter Temperature, Degrees F	73.8	80.1
Vmstd	Sampled Volume of Source Gas, Dry SCF	40.396	36.424
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.144	1.031
Vlc	Volume of Condensed Liquid, mL	158.1	188.7
Vwstd	Volume of Water Vapor, SCF	7.441	8.881
%H2O	Moisture Content, Percent by Volume	15.6	19.6
%H2Osat	Saturated Moisture Content, Percent by Volume	100	100
Mfd	Source Gas Dry Mole Fraction	0.844	0.804
%CO2	Source Gas CO2 Content, Percent by Dry Volume	8.3	8.5
%O2	Source Gas O2 Content, Percent by Dry Volume	11.2	11.4
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.8	29.8
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	27.9	27.5
Pg	Source Gas Static Pressure, Inches H2O	-2.60	-17.0
Ps	Source Gas Absolute Pressure, Inches Hg	29.3	28.3
ts	Source Gas Temperature, Degrees F	442.0	268.1
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.691	0.982
vs	Source Gas Velocity, Feet/Second	62.6	68.9
A	Source Cross Sectional Area, Square Inches	3,025	2,627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	38,228	41,502
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,083	1,175
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	78,948	75,393
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,236	2,135
%I	Average Isokinetic Sampling Rate, Percent	104	103
Fo	Fuel Factor	1.17	1.12

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>1-I-MM101A-4</u>	<u>1-O-MM101A-4</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	153.6	25.2
ppmvd	Concentration, Parts per Million by Volume Dr	0.01610	0.00293
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.0231	0.00428
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.0233	0.00413
ug/DSCM	Concentration, Micrograms per DSCM	134.3	24.4
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	192.4	35.7
ug/DSCM@12%CO	Concentration, ug/DSCM @ 12% CO2	194.1	34.4
lb/hr	Emission Rate, Pounds per Hour	0.01923	0.00379
g/sec	Emission Rate, Grams Per Second	0.00242	0.000478

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA

Test Location: UNIT No. 1

Run Number	Run Date	Operator
1-I-MM101A-5	3/20/98	ALFRED GUSMAN
1-O-MM101A-5	3/20/98	WAYNE JOHNSON

		<u>1-I-MM101A-5</u>	<u>1-O-MM101A-5</u>
	Run Start Time	1024	1030
	Run Stop Time	1135	1133
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.255	0.217
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	1.0138	0.9757
Pbar	Barometric Pressure, Inches Hg	29.5	29.5
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.46	1.28
Vm	Sampled Volume of Source Gas, Dry ACF	40.954	39.148
Vmm	Sampled Volume of Source Gas, Dry ACM	1.160	1.109
tm	Dry Gas Meter Temperature, Degrees F	78.3	84.7
Vmstd	Sampled Volume of Source Gas, Dry SCF	40.299	36.622
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.141	1.037
Vlc	Volume of Condensed Liquid, mL	145.1	191.9
Vwstd	Volume of Water Vapor, SCF	6.829	9.032
%H2O	Moisture Content, Percent by Volume	14.5	19.8
%H2Osat	Saturated Moisture Content, Percent by Volume	100	100
Mfd	Source Gas Dry Mole Fraction	0.855	0.802
%CO2	Source Gas CO2 Content, Percent by Dry Volume	8.5	8.3
%O2	Source Gas O2 Content, Percent by Dry Volume	10.8	11.2
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.8	29.8
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.1	27.4
Pg	Source Gas Static Pressure, Inches H2O	-2.60	-17.0
Ps	Source Gas Absolute Pressure, Inches Hg	29.3	28.3
ts	Source Gas Temperature, Degrees F	449.8	287.8
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.700	1.043
vs	Source Gas Velocity, Feet/Second	63.2	72.0
A	Source Cross Sectional Area, Square Inches	3,025	2,627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	38,707	42,168
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,096	1,194
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	79,621	78,852
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,255	2,233
%I	Average Isokinetic Sampling Rate, Percent	103	103
Fo	Fuel Factor	1.19	1.17

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>1-I-MM101A-5</u>	<u>1-O-MM101A-5</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	67.9	17.5
ppmvd	Concentration, Parts per Million by Volume Dr	0.00713	0.00202
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.00982	0.00290
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.0101	0.00293
ug/DSCM	Concentration, Micrograms per DSCM	59.5	16.9
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	81.9	24.2
ug/DSCM@12%CO	Concentration, ug/DSCM @ 12% CO2	84.0	24.4
lb/hr	Emission Rate, Pounds per Hour	0.00862	0.00267
g/sec	Emission Rate, Grams Per Second	0.00109	0.000336

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA
 Test Location: UNIT No. 1

<u>Run Number</u>	<u>Run Date</u>	<u>Operator</u>
1-I-MM101A-6	3/20/98	ALFRED GUSMAN
1-O-MM101A-6	3/20/98	WAYNE JOHNSON

		<u>1-I-MM101A-6</u>	<u>1-O-MM101A-6</u>
	Run Start Time	1200	1200
	Run Stop Time	1305	1303
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.256	0.218
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	1.0138	0.9757
Pbar	Barometric Pressure, Inches Hg	29.5	29.5
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.52	1.23
Vm	Sampled Volume of Source Gas, Dry ACF	41.336	39.173
Vmm	Sampled Volume of Source Gas, Dry ACM	1.171	1.109
tm	Dry Gas Meter Temperature, Degrees F	80.9	87.8
Vmstd	Sampled Volume of Source Gas, Dry SCF	40.487	36.434
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.146	1.032
Vlc	Volume of Condensed Liquid, mL	161.7	185.5
Vwstd	Volume of Water Vapor, SCF	7.610	8.731
%H2O	Moisture Content, Percent by Volume	15.8	19.3
%H2Osat	Saturated Moisture Content, Percent by Volume	100	100
Mfd	Source Gas Dry Mole Fraction	0.842	0.807
%CO2	Source Gas CO2 Content, Percent by Dry Volume	8.6	8.2
%O2	Source Gas O2 Content, Percent by Dry Volume	11.0	11.3
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.8	29.8
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	27.9	27.5
Pg	Source Gas Static Pressure, Inches H2O	-2.80	-17.0
Ps	Source Gas Absolute Pressure, Inches Hg	29.3	28.3
ts	Source Gas Temperature, Degrees F	449.5	289.8
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.716	1.019
vs	Source Gas Velocity, Feet/Second	64.0	71.2
A	Source Cross Sectional Area, Square Inches	3,025	2,627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	38,624	41,810
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,094	1,184
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	80,726	77,951
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,286	2,207
%I	Average Isokinetic Sampling Rate, Percent	103	102
Fo	Fuel Factor	1.15	1.17

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>1-I-MM101A-6</u>	<u>1-O-MM101A-6</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	944.6	17.1
ppmvd	Concentration, Parts per Million by Volume Dr	0.0988	0.00199
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.139	0.00288
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.138	0.00291
ug/DSCM	Concentration, Micrograms per DSCM	824	16.6
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	1157	24.0
ug/DSCM@12%CO	Concentration, ug/DSCM @ 12% CO2	1150	24.3
lb/hr	Emission Rate, Pounds per Hour	0.119	0.00260
g/sec	Emission Rate, Grams Per Second	0.0150	0.000327

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA
 Test Location: UNIT No. 1

<u>Run Number</u>	<u>Run Date</u>	<u>Operator</u>
1-I-MM101-7	3/20/98	ALFRED GUSMAN
1-O-MM101A-7	3/20/98	WAYNE JOHNSON

		<u>1-I-MM101-7</u>	<u>1-O-MM101A-7</u>
	Run Start Time	1332	1332
	Run Stop Time	1437	1437
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.255	0.217
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	1.0138	0.9757
Pbar	Barometric Pressure, Inches Hg	29.5	29.5
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.39	1.24
Vm	Sampled Volume of Source Gas, Dry ACF	39.678	38.830
Vmm	Sampled Volume of Source Gas, Dry ACM	1.124	1.100
tm	Dry Gas Meter Temperature, Degrees F	80.8	87.3
Vmstd	Sampled Volume of Source Gas, Dry SCF	38.856	36.149
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.100	1.024
Vlc	Volume of Condensed Liquid, mL	159.0	181.8
Vwstd	Volume of Water Vapor, SCF	7.483	8.556
%H2O	Moisture Content, Percent by Volume	16.1	19.1
%H2Osat	Saturated Moisture Content, Percent by Volume	100	100
Mfd	Source Gas Dry Mole Fraction	0.839	0.809
%CO2	Source Gas CO2 Content, Percent by Dry Volume	9.6	8.3
%O2	Source Gas O2 Content, Percent by Dry Volume	10.1	11.4
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.9	29.8
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.0	27.5
Pg	Source Gas Static Pressure, Inches H2O	-2.80	-17.0
Ps	Source Gas Absolute Pressure, Inches Hg	29.3	28.3
ts	Source Gas Temperature, Degrees F	444.2	288.3
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.662	1.005
vs	Source Gas Velocity, Feet/Second	61.3	70.6
A	Source Cross Sectional Area, Square Inches	3,025	2,627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	37,066	41,647
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,050	1,179
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	77,317	77,309
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,189	2,189
%I	Average Isokinetic Sampling Rate, Percent	103	103
Fo	Fuel Factor	1.13	1.14

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>1-I-MM101-7</u>	<u>1-O-MM101A-7</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	491.4	26.7
ppmvd	Concentration, Parts per Million by Volume Dr	0.0536	0.00313
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.0689	0.00458
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.0669	0.00453
ug/DSCM	Concentration, Micrograms per DSCM	447	26.1
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	575	38.2
ug/DSCM@12%CO	Concentration, ug/DSCM @ 12% CO2	558	37.7
lb/hr	Emission Rate, Pounds per Hour	0.0620	0.00407
g/sec	Emission Rate, Grams Per Second	0.00781	0.000513

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LEE, INC., FORT MYERS, FLORIDA

Test Location: UNIT No. 1 OUTLET

<u>Run Number</u>	<u>Run Date</u>	<u>Operator</u>
1-O-M26-1	3/20/98	SHAWN GRAHAM

		<u>1-O-M26-1</u>
	Run Start Time	1402
	Run Stop Time	1447
	Net Sampling/Traversing Points	9.0
	Net Run Time, Minutes	45
Y	Dry Gas Meter Calibration Coefficient	1.0053
Pbar	Barometric Pressure, Inches Hg	29.5
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.8
Vm	Sampled Volume of Source Gas, Dry ACF	35.553
Vmm	Sampled Volume of Source Gas, Dry ACM	1.007
tm	Dry Gas Meter Temperature, Degrees F	79.2
Vmstd	Sampled Volume of Source Gas, Dry SCF	34.661
Vmstdm	Sampled Volume of Source Gas, Dry SCM	0.981
%H ₂ O	Moisture Content, Percent by Volume	19.1
%CO ₂	Source Gas CO2 Content, Percent by Dry Volume	8.3
%O ₂	Source Gas O2 Content, Percent by Dry Volume	11.4
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.8
Pg	Source Gas Static Pressure, Inches H2O	-17.0
Ps	Source Gas Absolute Pressure, Inches Hg	28.3
A	Source Cross Sectional Area, Square Inches	2627

Note:

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)

		<u>1-O-M26-1</u>
	<u>Hydrogen Chloride</u>	
FWt	Formula Weight, Lb/Lb-Mole	36.5
ug	Catch Weight, Micrograms	44,300
	<u>Chlorine</u>	
ug	Catch Weight, Micrograms	182
ug	Catch Weight, Micrograms (from HCl Catch)	86,355
ppmvd	Concentration, Parts Per Million by Volume Dry	58.0
ppmvd@7%O ₂	Concentration, ppmvd @ 7% O ₂	84.8
ppmvd@12%C	Concentration, ppmvd @ 12% CO ₂	83.8

APPENDIX A
RESULTS TABULATION

2.0 UNIT NO. 2

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA
 Test Location: UNIT No.2

<u>Run Number</u>	<u>Run Date</u>	<u>Operator</u>
2-I-M101A-1	03/18/98	ALFRED GUSMAN
2-O-M101A-1	03/18/98	WAYNE JOHNSON

		<u>2-I-M101A-1</u>	<u>2-O-M101A-1</u>
	Run Start Time	1616	1616
	Run Stop Time	1728	1719
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.256	0.219
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	1.0138	0.9757
Pbar	Barometric Pressure, Inches Hg	29.8	29.8
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.36	1.13
Vm	Sampled Volume of Source Gas, Dry ACF	39.304	37.115
Vmm	Sampled Volume of Source Gas, Dry ACM	1.113	1.051
tm	Dry Gas Meter Temperature, Degrees F	82.7	90.4
Vmstd	Sampled Volume of Source Gas, Dry SCF	38.741	34.696
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.097	0.982
Vlc	Volume of Condensed Liquid, mL	115.8	115.6
Vwstd	Volume of Water Vapor, SCF	5.450	5.441
%H2O	Moisture Content, Percent by Volume	12.3	13.6
%H2Osat	Saturated Moisture Content, Percent by Volume	100	100
Mfd	Source Gas Dry Mole Fraction	0.877	0.864
%CO2	Source Gas CO2 Content, Percent by Dry Volume	8.4	8.3
%O2	Source Gas O2 Content, Percent by Dry Volume	11.7	12.0
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.8	29.8
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.4	28.2
Pg	Source Gas Static Pressure, Inches H2O	-1.70	-17.0
Ps	Source Gas Absolute Pressure, Inches Hg	29.7	28.6
ts	Source Gas Temperature, Degrees F	421.5	282.2
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.618	0.868
vs	Source Gas Velocity, Feet/Second	57.8	64.2
A	Source Cross Sectional Area, Square Inches	3,025	2,627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	37,930	41,260
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,074	1,168
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	72,829	70,312
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,062	1,991
%I	Average Isokinetic Sampling Rate, Percent	100.0	97.7
Fo	Fuel Factor	1.10	1.07

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>2-I-M101A-1</u>	<u>2-O-M101A-1</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	105.2	10.10
ppmvd	Concentration, Parts per Million by Volume Dr	0.0115	0.001233
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.0174	0.00193
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.0164	0.00178
ug/DSCM	Concentration, Micrograms per DSCM	95.9	10.28
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	145	16.1
ug/DSCM@12%CO	Concentration, ug/DSCM @ 12% CO2	137	14.9
lb/hr	Emission Rate, Pounds per Hour	0.0136	0.00159
g/sec	Emission Rate, Grams Per Second	0.00172	0.000200

* - The catch weight was corrected for the reagent blank analytical results.

FIELD DATA AND RESULTS TABULATION

Plant: OGDEN MARTIN SYSTEMS OF LAKE, INC., OKAHUMPKA, FLORIDA
 Test Location: UNIT No.2

<u>Run Number</u>	<u>Run Date</u>	<u>Operator</u>
2-I-MM101A-1	03/18/98	ALFRED GUSMAN
2-O-MM101A-1	03/18/98	WAYNE JOHNSON

		<u>2-I-MM101A-1</u>	<u>2-O-MM101A-1</u>
	Run Start Time	1758	1803
	Run Stop Time	1912	1912
	Net Sampling/Traversing Points	24	24
	Net Run Time, Minutes	60	60
Dia	Nozzle Diameter, Inches	0.255	0.216
Cp	Pitot Tube Coefficient	0.84	0.84
Y	Dry Gas Meter Calibration Coefficient	1.0138	0.9757
Pbar	Barometric Pressure, Inches Hg	29.8	29.8
Delta-H	Orifice Average Pressure Differential, Inches H2O	1.34	1.14
Vm	Sampled Volume of Source Gas, Dry ACF	38.825	37.195
Vmm	Sampled Volume of Source Gas, Dry ACM	1.099	1.053
tm	Dry Gas Meter Temperature, Degrees F	79.4	86.5
Vmstd	Sampled Volume of Source Gas, Dry SCF	38.501	35.020
Vmstdm	Sampled Volume of Source Gas, Dry SCM	1.090	0.992
Vlc	Volume of Condensed Liquid, mL	128.8	132.8
Vwstd	Volume of Water Vapor, SCF	6.062	6.250
%H2O	Moisture Content, Percent by Volume	13.6	15.1
%H2Osat	Saturated Moisture Content, Percent by Volume	100	100
Mfd	Source Gas Dry Mole Fraction	0.864	0.849
%CO2	Source Gas CO2 Content, Percent by Dry Volume	8.2	8.3
%O2	Source Gas O2 Content, Percent by Dry Volume	11.4	12.0
Md	Source Gas Dry Molecular Weight, Lb/Lb-Mole	29.8	29.8
Ms	Source Gas Wet Molecular Weight, Lb/Lb-Mole	28.2	28.0
Pg	Source Gas Static Pressure, Inches H2O	-2.50	-17.0
Ps	Source Gas Absolute Pressure, Inches Hg	29.6	28.6
ts	Source Gas Temperature, Degrees F	424.8	281.9
Delta-p	Source Gas Average Velocity Head, Inches H2O	0.625	0.931
vs	Source Gas Velocity, Feet/Second	58.5	66.7
A	Source Cross Sectional Area, Square Inches	3,025	2,627
Qsd	Source Gas Volumetric Flow Rate, Dry SCFM	37,609	42,089
Qmsd	Source Gas Volumetric Flow Rate, Dry SCMM	1,065	1,192
Qaw	Source Gas Volumetric Flow Rate, Wet ACFM	73,694	73,039
Qmaw	Source Gas Volumetric Flow Rate, Wet ACMM	2,087	2,068
%I	Average Isokinetic Sampling Rate, Percent	101.1	99.4
Fo	Fuel Factor	1.16	1.07

All standard volumes and flow rates based on 68 Degrees F (20 Degrees C) -- 29.92 Inches of Mercury (Hg)
 The lesser of %H2O and %H2Osat was used for calculation purposes

FIELD DATA AND RESULTS TABULATION

		<u>2-I-MM101A-1</u>	<u>2-O-MM101A-1</u>
	<u>Mercury</u>		
FWt	Formula Weight, Lb/Lb-Mole	200.59	200.59
ug	Catch Weight, Micrograms *	150.6	7.45
ppmvd	Concentration, Parts per Million by Volume Dr	0.0166	0.000901
ppmvd@7%O2	Concentration, ppmvd @7% O2	0.0242	0.00141
ppmvd@12%CO2	Concentration, ppmvd @12% CO2	0.0242	0.00130
ug/DSCM	Concentration, Micrograms per DSCM	138	7.51
ug/DSCM@7%O2	Concentration, ug/DSCM @ 7% O2	202	11.7
ug/DSCM@12%CO	Concentration, ug/DSCM @ 12% CO2	202	10.9
lb/hr	Emission Rate, Pounds per Hour	0.0195	0.00118
g/sec	Emission Rate, Grams Per Second	0.00245	0.000149

* - The catch weight was corrected for the reagent blank analytical results.

APPENDIX B
EXAMPLE CALCULATIONS

FIELD DATA AND RESULTS TABULATION

EXAMPLE CALCULATIONS, RUN 1-I-MM101A-1

SAMPLED VOLUME OF SOURCE GAS, DRY ACTUAL CUBIC FEET

$$\begin{aligned} V_{mm} &= V_m * 0.028317 \\ &= 41.000 * 0.028317 \\ &= 1.16 \end{aligned}$$

SAMPLED VOLUME OF SOURCE GAS, DRY STANDARD CUBIC FEET

$$\begin{aligned} V_{mstd} &= [(T_{std} + 460)/P_{std}] * Y * V_m * (P_{bar} + \Delta H/13.6) / (460 + t_m) \\ &= [(68 + 460)/29.92] * 1.0138 * 41.000 * (29.60 + 1.55/13.6) / (460 + 74) \\ &= 40.793 \end{aligned}$$

SAMPLED VOLUME OF SOURCE GAS, DRY STANDARD CUBIC METER

$$\begin{aligned} V_{mstdm} &= V_{mstd} * 0.028317 \\ &= 40.793 * 0.028317 \\ &= 1.155 \end{aligned}$$

VOLUME OF WATER VAPOR, STANDARD CUBIC FEET

$$\begin{aligned} V_{wstd} &= 0.002667 * [(T_{std} + 460) / P_{std}] * V_{lc} \\ &= 0.002667 * [(68 + 460) / 29.92] * 148.3 \\ &= 6.980 \end{aligned}$$

MOISTURE CONTENT, PERCENT BY VOLUME

$$\begin{aligned} \%H_2O &= V_{wstd} / (V_{wstd} + V_{mstd}) \\ &= 6.980 / (6.980 + 40.793) \\ &= 14.61 \end{aligned}$$

DRY MOLE FRACTION, LB-MOLE/LB-MOLE

$$\begin{aligned} M_{fd} &= 1 - \%H_2O/100 \\ &= 1 - 14.61/100 \\ &= 0.854 \end{aligned}$$

DRY MOLECULAR WEIGHT, LB/LB-MOLE

$$\begin{aligned} M_d &= 44 * (\%CO_2/100) + 32 * (\%O_2/100) + 28 * \{[100 - (\%CO_2 + \%O_2)]/100\} \\ &= 44 * (8.4/100) + 32 * (11.3/100) + 28 * \{[100 - (8.4 + 11.3)]/100\} \\ &= 29.80 \end{aligned}$$

WET MOLECULAR WEIGHT, LB/LB-MOLE

$$\begin{aligned} M_s &= M_d * M_{fd} + 18.0 * \%H_2O/100 \\ &= 29.80 * 0.854 + 18.0 * 14.61/100 \\ &= 28.07 \end{aligned}$$

ABSOLUTE PRESSURE, INCHES OF MERCURY

$$\begin{aligned} P_s &= P_{bar} + P_g/13.6 \\ &= 29.60 + -2.50/13.6 \\ &= 29.42 \end{aligned}$$

VELOCITY, FEET PER SECOND

$$\begin{aligned} v_s &= 85.49 * C_p * \text{SQRT}[\Delta p * (460 + t_s) / P_s / M_s] \\ &= 85.49 * 0.84 * \text{SQRT}[0.7373 * (460 + 451) / 29.42 / 28.07] \\ &= 64.77 \end{aligned}$$

FIELD DATA AND RESULTS TABULATION

VOLUMETRIC FLOW RATE, DRY STANDARD CUBIC FEET PER MINUTE

$$\begin{aligned} Q_{sd} &= (60/144) * M_{fd} * v_s * A * (T_{std} + 460)/(t_s + 460) * (P_s/P_{std}) \\ &= (60/144) * 0.854 * 64.77 * 3025 * (68 + 460)/(451 + 460) * (29.42/29.92) \\ &= 39719 \end{aligned}$$

VOLUMETRIC FLOW RATE, DRY STANDARD CUBIC METER PER MINUTE

$$\begin{aligned} Q_{msd} &= Q_{sd} * 0.028317 \\ &= 39719 * 0.028317 \\ &= 1125 \end{aligned}$$

VOLUMETRIC FLOW RATE, ACTUAL CUBIC FEET PER MINUTE

$$\begin{aligned} Q_{aw} &= (60/144) * v_s * A \\ &= (60/144) * 64.77 * 3025 \\ &= 81631 \end{aligned}$$

VOLUMETRIC FLOW RATE, ACTUAL CUBIC METER PER MINUTE

$$\begin{aligned} Q_{maw} &= Q_{aw} * 0.028317 \\ &= 81631 * 0.028317 \\ &= 2312 \end{aligned}$$

ISOKINETIC SAMPLING RATE, PERCENT

$$\begin{aligned} \%I &= P_{std}/(T_{std} + 460) * (100/60) * V_{mstd} * (t_s + 460) / [P_s * v_s * M_{fd} * \theta * (\pi * Dia * Dia / 576)] \\ &= 29.92 / (68 + 460) * (100/60) * 40.793 * (451 + 460) / [29.42 * 64.77 * 0.854 * 60.00 * (\pi * 0.256 * 0.256 / 576)] \\ &= 100.6 \end{aligned}$$

FUEL FACTOR

$$\begin{aligned} F_o &= (20.9 - \%O_2) / 20.9 \\ &= (20.9 - 11.3) / 20.9 \\ &= 1.143 \end{aligned}$$

FIELD DATA AND RESULTS TABULATION

MERCURY CONCENTRATION, PARTS PER MILLION BY VOLUME DRY

$$\begin{aligned}\text{ppmvd} &= (\text{Catch/Conversion}) * 385.3 * 1,000,000 / 453.592 / \text{FWt} / \text{Vmstd} * (460 + \text{Tstd}) / 528 \\ &= (69.7/1000000) * 385.3 * 1,000,000 / 453.592 / 200.59 / 40.793 * (460 + 68) / 528 \\ &= 0.00724\end{aligned}$$

MERCURY CONCENTRATION, PARTS PER MILLION BY VOLUME DRY @ 7% O2

$$\begin{aligned}\text{ppm@7\%O2} &= \text{ppmvd} * (20.9 - 7) / (20.9 - \%O2) \\ &= 0.0072 * (20.9 - 7) / (20.9 - 11.3) \\ &= 0.01048\end{aligned}$$

MERCURY CONCENTRATION, PARTS PER MILLION BY VOLUME DRY @ 12% CO2

$$\begin{aligned}\text{ppm@12\%CO2} &= \text{ppmvd} * 12 / \%CO2 \\ &= 0.0072 * 12 / 8.4 \\ &= 0.01034\end{aligned}$$

MERCURY CONCENTRATION, MICROGRAMS PER DRY STANDARD CUBIC METER

$$\begin{aligned}\text{ug/DSCM} &= (\text{Catch/Conversion}) * 1,000,000 / \text{Vmstdm} \\ &= (70/1000000) * 1,000,000 / 1.155 \\ &= 60.4\end{aligned}$$

MERCURY CONCENTRATION, MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2

$$\begin{aligned}\text{ug/DSCM@7\%O2} &= \text{ug/DSCM} * (20.9 - 7) / (20.9 - \%O2) \\ &= (60 * 1,000,000 / 1.155 * (20.9 - 7) / (20.9 - 11.3)) \\ &= 87.4\end{aligned}$$

MERCURY CONCENTRATION, NANOGRAMS PER DRY STANDARD CUBIC METER @ 12% CO2

$$\begin{aligned}\text{ug/DSCM@12\%CO2} &= \text{ug/DSCM} * (12 / \%CO2) \\ &= (60 * (12/8.4)) \\ &= 86.2\end{aligned}$$

MERCURY EMISSION RATE, POUNDS PER HOUR

$$\begin{aligned}\text{lb/hr} &= 60 * (\text{Catch/Conversion}) * \text{Qsd} / 453.592 / \text{Vmstd} \\ &= 60 * (70/1000000) * 39719 / 453.592 / 40.793 \\ &= 0.00898\end{aligned}$$

MERCURY EMISSION RATE, GRAMS PER SECOND

$$\begin{aligned}\text{g/sec} &= (\text{Catch/Conversion}) * \text{Qsd} / 60 / \text{Vmstd} \\ &= 69.74/1000000 * 39719 / 60 / 40.793 \\ &= 0.001132\end{aligned}$$

APPENDIX C

FIELD DATA

1.0 UNIT NO. 1

a. INLET

METHOD 3 (ORSAT) FIELD DATA

Client ODDEN ENERGY
 Plant Name DMS LAKE
 City/State OKATOMPKA, FL
 Sampling Location UNIT No. 1 INLET

Job No. 10388
 Fuel Type MUNIWASTE

Run/Sample No. <u>1-I-M3-1</u> Date <u>3/19/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1010	1236	8.3	19.9	—	11.6	—	
1	1242	8.5	19.6	—	11.1	—	
1123	1249	8.5	19.7	—	11.2	—	
Avg.		8.4	Avg.		11.3	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B100</u>		F ₀ _____			

Run/Sample No. <u>1-I-m3-2</u> Date <u>3/19/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1355	1550	8.5	19.6	—	11.1	—	
1	1558	8.3	19.5	—	11.2	—	
1502	1605	8.3	19.5	—	11.2	—	
Avg.		8.4	Avg.		11.2	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B200</u>		F ₀ _____			

Run/Sample No. <u>1-I-M101A/M3-4</u> Date <u>3/20/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
0933	1115	8.4	19.5	—	11.1	—	
1	1125	8.3	19.5	—	11.2	—	
0943	1135	8.3	19.5	—	11.2	—	
Avg.		8.3	Avg.		11.2	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B14B</u>		F ₀ _____			

METHOD 3 (ORSAT) FIELD DATA

Client Olden
 Plant Name OMS LAKE
 City/State OKAHAWKA, FL
 Sampling Location UNIT No. 1 NCE

Job No. 10388
 Fuel Type MUNI WASTE

Run/Sample No. <u>1-I-mm101A/m3-5</u> Date <u>3/20/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1030	1225	8.5	19.3	—	10.8	—	
1	1232	8.5	19.3	—	10.8	—	
1135	1240	8.5	19.3	—	10.8	—	
Avg.		8.5	Avg.		10.8	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B139</u>		F ₀ _____			

Run/Sample No. <u>1-I-mm101A/m3-6</u> Date <u>3/20/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1200	1336	8.6	19.5	—	10.9	—	
1	1343	8.6	19.6	—	11.0	—	
1305	1350	8.6	19.6	—	11.0	—	
Avg.		8.6	Avg.		11.0	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B148</u>		F ₀ _____			

Run/Sample No. <u>1-I-mm101A/m3-7</u> Date <u>3/20/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1332	1508	9.5	19.6	—	10.1	—	
1	1520	9.7	19.8	—	10.1	—	
1437	1530	9.7	19.8	—	10.1	—	
Avg.		9.6	Avg.		10.1	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B200</u>		F ₀ _____			

SAMPLING DATA - METHOD (S) mod 101A

1 of 1

CLIENT: ODGE ENERGY GROUP, INC PLANT: ODGEN MARTIN SYSTEMS E, INC
 CITY/STATE: ORAHUMPKA, FL JOB NO.: 10588
 SAMPLE LOCATION: Unit I inlet RUN NO.: I-I-MML01A-1
 BAR. PRESS., IN. HG: 29.6 STATIC PRESSURE, IN. H₂O: -2.5 DATE: 3-19-98
 LEAK ✓ VAC., IN. HG: 15 15 RUN TIME: 1010 - 1123
 LEAK RATE, CFM: 0.000 0.001 TEST PERSONS: AS DB

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS		NOMOGRAPH		FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@		XAD	WT.
PITOT	✓		<u>2109</u>	<u>1.0894</u>	<u>1.712</u>			
TC	✓	✓	PITOT ID <u>PT12</u>	Cp <u>0.94</u>	METER TEMP. <u>85</u>			
NOZZLE	✓	✓	TC READOUT <u>2109</u>	TC <u>0.290</u>	EST. % H ₂ O <u>12</u>			
ORSAT	✓	NA	NOZZLE NO. <u>GN2007</u>	DIA. <u>0.256</u>	"C" FACTOR <u>0.821</u>			
			SAMPLE BOX <u>05</u>	REAGNT. <u>632755</u>	STACK TEMP. <u>450</u>			
			UMBILICAL		REF DELTA-P <u>0.863</u>			
			ORSAT PUMP <u>022</u>	BAG <u>B100</u>	"K" FACTOR <u>2.133</u>			

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-1	0	464.1	0.56	70	432	1.2	1.185	4	331	68	NA
2	2	2 1/2	465.79	0.75	69	447	1.55	1.858	5	320	68	
3	3	5	467.45	0.91	69	454	1.9	1.874	6	330	68	
4	4		469.265	0.83	71	465	1.7	1.710	5.5	321	66	
5	5	10	471.08	0.82	71	458	1.7	1.687	6	320	69	
6	6		472.84	0.79	72	459	1.6	1.626	7	322	68	
7	7	15	474.62	0.8	72	454	1.65	1.647	7	327	67	
8	8		476.39	0.78	73	458	1.6	1.611	7.5	328	67	
9	B-1	20	478.155	0.65	72	439	1.75	1.760	8	351	67	
10	2		479.765	0.68	74	449	1.4	1.422	8	347	66	
11	3	25	481.385	0.67	74	455	1.4	1.392	9	342	67	
12	4		483.07	0.65	74	455	1.38	1.350	10	343	67	
13	5	30	484.7	0.7	75	456	1.45	1.455	10	355	66	
14	6		486.38	0.76	76	455	1.6	1.581	12	349	61	
15	7	35	488.055	0.8	77	454	1.7	1.672	13.5	341	62	
16	8		489.86	0.81	77	454	1.7	1.643	13.5	339	62	
17	C 1	40	491.651	0.53	74	428	1.15	1.134	11	338	62	
18	2		493.205	0.71	75	441	1.5	1.501	10	335	52	
19	3	45	494.85	0.76	76	453	1.6	1.588	11	331	53	
20	4		496.66	0.68	77	453	1.4	1.423	12	327	53	
21	5	50	498.4	0.7	78	452	1.6	1.470	13.5	330	56	
22	6		500.68	0.8	78	452	1.7	1.679	13.5	331	56	
23	7	55	501.69	0.8	79	453	1.7	1.660	14	329	56	
24	8		503.34	0.82	80	450	1.7	1.725	15	328	54	
25	END	60	505.1									

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REVIEWER

60 41.000 1.7373 74.3 451.0 1.55

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SAMPLING DATA - METHOD (S) MM101A

Page 1 of 1

CLIENT: OGDEN ENERGY GROUP, Inc PLANT: OGDEN MARTIN SYSTEMS OF LAKE, Inc
 CITY/STATE: ORLAHUMPKA, FL JOB NO.: 10388
 SAMPLE LOCATION: Unit 1 Inlet RUN NO.: 1-1-MM101A
 BAR. PRESS., IN. HG: 29.6 STATIC PRESSURE, IN. H₂O: -2.5 DATE: 3-19-98
 LEAK ✓ VAC., IN. HG: 15 13 RUN TIME: 1355 - 1502
 LEAK RATE, CFM: 0.000 0.000 TEST PERSONS: AG DB

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS			NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX			DELTA H@			XAD	WT.
PITOT	✓		<u>2108</u>	Y	<u>1.0138</u>	<u>1.712</u>				
TC	✓		PITOT ID <u>PT3</u>	Cp	<u>0.84</u>	METER TEMP.	<u>90</u>			
NOZZLE	✓		TC READOUT <u>2108</u>	TC	<u>7</u>	EST. % H ₂ O	<u>12</u>			
ORSAT	✓	NA	NOZZLE NO. <u>6N2010</u>	DIA	<u>0.256</u>	"C" FACTOR	<u>0.821</u>			
			SAMPLE BOX <u>09</u>	REAGNT.	<u>632/28</u>	STACK TEMP.	<u>443</u>			
			UMBILICAL			REF DELTA-P	<u>0.863</u>			
			ORSAT PUMP <u>OR2</u>	BAG	<u>B200</u>	"K" FACTOR	<u>2.133</u>			

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-1	0	505.321	0.64	75	435	1.35	1.363	2	331	58	NA
2	2	2 1/2	507.034	0.82	75	450	1.7	1.716	4	333	58	
3	3	5	506.83	0.81	75	459	1.7	1.677	4	331	58	
4	4	7 1/2	510.691	0.79	75	459	1.65	1.636	5	330	58	
5	5	10	512.46	0.77	76	459	1.6	1.597	5.5	327	58	
6	6		511.22	0.4	77	458	1.65	1.665	5.5	327	59	
7	7	15	515.96	0.74	77	459	1.65	1.642	6.5	327	58	
8	8		517.918	0.77	78	459	1.6	1.603	6.5	328	58	
9	B-9	20	519.62	0.63	77	459	1.35	1.354	6	330	59	
10	2		521.327	0.66	77	445	1.4	1.394	6	330	59	
11	3	25	522.94	0.68	78	459	1.4	1.417	7	328	59	
12	4		524.65	0.63	78	460	1.3	1.311	7	324	59	
13	5	30	526.28	0.71	78	460	1.5	1.474	7.5	332	55	
14	6		527.475	0.77	79	459	1.6	1.607	8	330	58	
15	7	35	529.255	0.62	79	461	1.7	1.707	9	330	58	
16	8		531.62	0.83	80	458	1.7	1.736	9.5	327	55	
17	C-1	40	533.461	0.46	77	410	1	1.010	8	330	58	
18	2		534.91	0.65	78	424	1.4	1.409	9	328	57	
19	3	45	536.67	0.66	78	457	1.4	1.387	9	331	59	
20	4		538.34	0.62	78	449	1.3	1.306	9.5	321	59	
21	5	50	539.978	0.65	78	445	1.4	1.376	10	327	60	
22	6		541.64	0.71	79	446	1.5	1.503	10.5	325	60	
23	7	55	543.36	0.74	79	445	1.5	1.586	11	304	60	
24	8		545.01	0.81	80	445	1.7	1.719	12	320	60	
25	EAD	60	546.441									

FINAL

REVIEWER

60 41.520 0.7145 77.5 449.3 1.50

SAMPLING DATA - METHOD (S) MM101A

CLIENT: DODEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORAHUMOKA, FC JOB NO.: 10388
 FILE LOCATION: UNIT 1 Inlet RUN NO.: 1-I-mm1014-4
 BAR. PRESS., IN. HG: 29.5 STATIC PRESSURE, IN. H₂O: -2.6 DATE: 3-20-98
 LEAK ✓ VAC., IN. HG: 15 17 RUN TIME: 833 - 943
 LEAK RATE, CFM: 0.009 0.014 TEST PERSONS: AG DB

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX		Y	DELTA H@			XAD	WT.	
PITOT	✓	✓	2108		10134	1.712					
TC	✓	✓	PITOT ID 24		Cp 0.84	METER TEMP. 90					
NOZZLE	✓	✓	TC READOUT 2108		TC 7	EST. % H ₂ O 12					
ORSAT	✓	NA	NOZZLE NO. 617010		DIA. 0.256	"C" FACTOR 0.821					
			SAMPLE BOX 08		REAQNT. 207/611	STACK TEMP. 450					
			UMBILICAL			REF DELTA-P 0.863					
			ORSAT PUMP 022		BAGB148	"K" FACTOR 2.133					

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-1	0	559.74	0.51	71	414	1.1	1.104	3	314	68	N/A
2	2		556.305	0.7	71	429	1.5	1.484	4	315	68	
3	3	5	558.005	0.76	71	446	1.6	1.578	5	308	68	
4	4		559.71	0.8	72	445	1.7	1.680	6	313	68	
5	5	10	561.555	0.64	72	446	1.45	1.041	6	310	68	
6	6		563.32	0.74	75	447	1.55	1.548	6	311	68	
7	7	15	565.06	0.75	73	448	1.55	1.566	7	310	67	
8	8		566.8	0.73	74	447	1.5	1.521	7	305	67	
9	B-1	20	564.464	0.56	73	420	1.2	1.207	6.5	309	61	
10	2		564.48	0.61	74	433	1.3	1.294	6.5	311	61	
11	3	25	571.6	0.63	74	444	1.3	1.325	8	304	58	
12	4		573.205	0.6	75	449	1.25	1.257	8.5	308	58	
13	5	30	574.8	0.64	74	456	1.45	1.442	9	311	59	
14	6		576.52	0.75	75	453	1.55	1.564	10.5	310	59	
15	7	35	578.213	0.77	75	453	1.6	1.605	11	313	59	
16	8		580	0.77	76	453	1.6	1.609	11	307	58	
17	C-1	40	581.774	0.51	74	400	1.1	1.126	9	311	58	
18	2		583.29	0.65	74	430	1.4	1.384	10	308	62	
19	3	45	584.93	0.67	75	449	1.4	1.403	11	307	61	
20	4		586.574	0.66	75	452	1.4	1.378	12.5	311	62	
21	5	50	588.25	0.7	75	451	1.45	1.463	13	312	62	
22	6		589.44	0.61	75	451	1.4	1.463	14	308	62	
23	7	55	591.744	0.74	75	450	1.55	1.547	16	310	62	
24	8		593.57	0.85	75	448	1.8	1.782	16	312	63	
END	60		595.444									

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REVIEWER

60 40.709 0.6908 73.9 442.3 1.46

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SAMPLING DATA - METHOD (S) MM101A

Page 1 of 1

CLIENT: OGDEN ENERGY GROUP, INC PLANT: OGDEN MARTIN SYSTEMS OF LAKE, INC
 CITY/STATE: OKLAHOMA, FL JOB NO.: 10388
 SAMPLE LOCATION: UNIT 1 Inlet RUN NO.: I-I-MM101A-5
 BAR. PRESS., IN. HG: 29.5 STATIC PRESSURE, IN. H₂O: -2.6 DATE: 3-20-98
 LEAK ✓ VAC., IN. HG: 15 13 RUN TIME: 1024 - 1135
 LEAK RATE, CFM: 0.01 0.60 TEST PERSONS: _____

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX		Y	DELTA H ₂ O			XAD	WT.	
PITOT	✓	✓	<u>2108</u>		<u>1.0138</u>	<u>1.717</u>					
TC	✓	✓	PITOT ID <u>12</u>	Cp	<u>0.84</u>	METER TEMP. <u>90</u>					
NOZZLE	✓	✓	TC READOUT <u>2104</u>	TC	<u>2280</u>	EST. % H ₂ O <u>12</u>					
ORSAT	✓	NA	NOZZLE NO. <u>6K12003</u>	DIA.	<u>0.255</u>	"C" FACTOR <u>0.814</u>					
			SAMPLE BOX <u>05</u>	REAGNT.	<u>6K1205</u>	STACK TEMP. <u>450</u>					
			UNBILICAL _____			REF DELTA-P <u>0.378</u>					
			ORSAT PUMP <u>0122</u>	BAG	<u>2134</u>	"K" FACTOR <u>2.095</u>					

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

PT. NO.	ELAPSED TIME, MINUTES	DCM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DCM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-1	0	595.7	0.54	75	428	1.15	1.138	3	276	68	NA
2	2		597.3	0.79	75	452	1.6	1.621	3.5	300	68	
3	3	5	594.04	0.73	75	450	1.5	1.449	4.5	301	66	
4	4		600.76	0.87	76	461	1.8	1.77	5	303	65	
5	5	10	602.66	0.86	77	462	1.75	1.748	5.5	301	62	
6	6		604.56	0.81	77	462	1.65	1.648	6	300	61	
7	7	15	606.3	0.78	77	461	1.6	1.589	6.5	301	60	
8	8		608.013	0.72	78	460	1.5	1.471	6.5	303	60	
9	B-1	20	609.831	0.51	77	437	1.05	1.067	6	311	60	
10	2		611.355	0.64	78	444	1.35	1.333	6.5	310	64	
11	3	25	613.045	0.62	78	450	1.3	1.282	7	314	64	
12	4		614.643	0.59	78	451	1.2	1.218	8	310	65	
13	5	30	616.13	0.68	79	454	1.4	1.402	8	316	68	
14	6		617.81	0.74	79	453	1.5	1.527	9	313	66	
15	7	35	619.58	0.77	79	452	1.6	1.590	10.5	310	66	
16	8		621.444	0.81	80	455	1.7	1.670	11	322	63	
17	C-1	40	623.319	0.46	78	420	1	0.98	9	316	67	
18	2		624.782	0.66	79	436	1.4	1.386	9	310	58	
19	3	45	626.355	0.68	80	451	1.4	1.409	10.5	316	56	
20	4		628.07	0.7	80	452	1.45	1.449	11	315	56	
21	5	50	629.72	0.71	81	451	1.5	1.474	12	317	60	
22	6		631.5	0.74	81	452	1.55	1.534	12.5	318	61	
23	7	55	633.36	0.69	81	450	1.45	1.434	12	315	64	
24	8		634.42	0.8	81	448	1.65	1.608	13	316	68	
25	END	60	636.654									

FINAL

REVIEWER

60 40.954 0.700L 78.3 449.0 1.146

SAMPLING DATA - METHOD (S) MM101A

CLIENT: OGDEN ENERGY GROUP, INC PLANT: OGDEN MARTIN SYSTEMS OF LAKE, INC
 CITY/STATE: ORAHUMPKA, FL JOB NO.: 10388
 SAMPLE LOCATION: Inlet Unit 1 RUN NO.: L-3-MM101A-6
 BAR. PRESS., IN. HG: 29.5 STATIC PRESSURE, IN. H₂O: ~ 2.8 DATE: 3-20-08
 LEAK ✓ VAC., IN. HG: 15 15 RUN TIME: 1200 - 1305
 LEAK RATE, CFM: 0.005 0.005 TEST PERSONS: 44 D.B

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@	DELTA H@			NAD	WT.	
PITOT	✓	J	PITOT ID	Cp	METER TEMP.	90					
TC	✓	✓	TC READOUT	TC	EST. % H ₂ O	12					
NOZZLE	✓	✓	NOZZLE NO.	DIA.	"C" FACTOR	0.819					
ORSAT	✓	NA	SAMPLE BOX	REAGNT.	STACK TEMP.	450					
			UMBILICAL		REF DELTA-P	0.865					
			ORSAT PUMP	BAG	"K" FACTOR	2.128					

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-1	0	636.44	6.65	78	420	1.4	1.412	6	266	67	NA
2	2		638.67	6.74	79	444	1.7	1.673	5	290	60	
3	3	5	640.48	6.8	79	452	1.7	1.678	4	300	60	
4	4		642.21	6.82	79	452	1.7	1.723	5	300	61	
5	5	10	644.05	6.76	80	451	1.6	1.588	5	307	61	
6	6		645.84	6.71	81	450	1.5	1.498	5.5	310	61	
7	7	15	647.53	6.72	81	451	1.5	1.519	5.5	313	62	
8	8		649.305	6.7	81	450	1.5	1.477	6	320	60	
9	B-4	20	650.958	6.54	80	432	1.15	1.160	6	320	60	
10	2		652.45	6.61	80	444	1.3	1.294	6	317	61	
11	3	25	654.06	6.64	80	449	1.35	1.380	7	314	58	
12	4		655.68	6.62	81	450	1.3	1.309	7	318	57	
13	5	30	657.32	6.7	81	452	1.5	1.474	8	317	55	
14	6		658.92	6.74	82	451	1.55	1.503	9	311	56	
15	7	35	660.7	6.81	82	453	1.7	1.706	9.5	312	57	
16	8		662.55	6.8	83	458	1.7	1.674	10	315	58	
17	C-1	40	664.351	6.66	81	440	1.4	1.407	9.5	316	58	
18	2		666.02	6.7	81	457	1.45	1.466	10	315	58	
19	3	45	667.66	6.69	81	460	1.45	1.440	10	308	60	
20	4		669.34	6.66	81	459	1.4	1.379	11	314	61	
21	5	50	671.065	6.77	82	456	1.6	1.618	11	311	61	
22	6		672.84	6.74	82	454	1.65	1.662	12	316	63	
23	7	55	674.545	6.73	82	452	1.55	1.539	13	314	63	
24	8		676.325	6.82	83	452	1.75	1.753	14	315	63	
END	60		678.181									

FINAL

REVIEWER

60 41.336 12.7160 80.9 449.5 1.52

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 SAMPLING DATA - METHOD (S) MM701A

CLIENT: OGDEN ENERGY GROUP, Inc PLANT: OGDEN MARTIN SYSTEMS OF LAKE, INC
 CITY/STATE: OKLAHOMA, FL JOB NO.: 10388
 SAMPLE LOCATION: Unit Inlet RUN NO.: 1-I-MM101A
 BAR. PRESS., IN. HG: 29.5 STATIC PRESSURE, IN. H₂O: -2.8 DATE: 3-20-98
 LEAK ✓ VAC., IN. HG: 15 15 RUN TIME: 1332-1437
 LEAK RATE, CFM: 0.005 0.005 TEST PERSONS: AG DB

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH		FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@		XAD	WT.		
PITOT	✓	✓	<u>2108</u>	<u>1.0138</u>	<u>1.712</u>					
TC	✓	✓	PITOT ID <u>12</u>	Cp <u>0.87</u>	METER TEMP. <u>90</u>					
NOZZLE	✓	✓	TC READOUT <u>2108</u>	TC <u>R280</u>	EST. % H ₂ O <u>12</u>					
ORSAT	✓	NA	NOZZLE NO. <u>6N203</u>	DIA. <u>0.255</u>	"C" FACTOR <u>0.818</u>					
			SAMPLE BOX <u>05</u>	REAGNT. <u>644/205</u>	STACK TEMP. <u>450</u>					
			UMBILICAL		REF DELTA-P <u>0.874</u>					
			ORSAT PUMP <u>OR 2</u>	BAG <u>B200</u>	"K" FACTOR <u>2.094</u>					

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

	PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	A-1	0	676.358	0.53	86	423	1.15	1.134	2.5	283	58	NA
2	2		679.98	0.68	80	440	1.4	1.427	4	280	58	
3	3	5	681.68	0.8	80	444	1.7	1.670	5	289	60	
4	4		683.51	0.65	80	444	1.35	1.386	6	287	61	
5	5	10	685.3	0.64	81	446	1.45	1.440	6	300	62	
6	6		686.93	0.68	82	446	1.4	1.421	6	301	62	
7	7	15	688.7	0.67	82	449	1.4	1.396	6	304	62	
8	8		690.25	0.65	82	447	1.35	1.357	6	304	61	
9	B-1	20	691.877	0.49	81	418	1.05	1.055	6	299	61	
10	2		693.39	0.61	81	440	1.3	1.282	6	305	61	
11	3	25	695.07	0.54	81	443	1.25	1.28	6.5	310	61	
12	4		696.82	0.56	81	444	1.2	1.171	7	314	64	
13	5	30	699.08	0.64	81	445	1.35	1.338	7	315	63	
14	6		699.67	0.71	81	447	1.5	1.480	7.5	310	63	
15	7	35	701.36	0.75	82	453	1.55	1.555	8	313	63	
16	8		703.045	0.77	81	452	1.6	1.585	9	318	63	
17	C-1	40	704.851	0.56	80	430	1.2	1.187	9	318	61	
18	2		706.335	0.65	80	442	1.35	1.360	8	316	60	
19	3	45	707.92	0.63	80	450	1.3	1.306	9	316	60	
20	4		709.57	0.72	80	449	1.5	1.445	10	309	61	
21	5	50	711.22	0.69	80	450	1.4	1.410	10.5	299	62	
22	6		712.02	0.73	81	456	1.5	1.506	11	300	60	
23	7	55	714.49	0.71	81	452	1.5	1.491	11	306	61	
24	8		716.33	0.8	74	450	1.65	1.695	11	312	61	
25	END	60	719.036									

FINAL

REVIEWER

60 39.678 0.6622 80.7 444.2 1.39

APPENDIX C

FIELD DATA

1.0 UNIT NO. 1

b. STACK

METHOD 3 (ORSAT) FIELD DATA

Client OGDEN ENERGY
 Plant Name OMS LAKE
 City/State OKLAHOMA, FL
 Sampling Location UNIT No. 1 OUTLET

Job No. 10388
 Fuel Type MUNICIPAL WASTE

Run/Sample No. <u>1-0-m3-1</u> Date <u>3/19/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator
							<u>SC6</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1010	1200	8.7	19.6	—	10.9	—	
1	1210	8.7	19.4	—	10.7	—	
1145	1220	8.7	19.5	—	10.8	—	
Avg.		8.7	Avg.		10.8	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B139</u>			F ₀ _____		

Run/Sample No. <u>1-0-m3-2</u> Date <u>3/19/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator
							<u>SC6</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1355	1512	8.6	20.0	—	11.4	—	
1	1522	8.6	20.0	—	11.4	—	
1459	1530	8.6	20.0	—	11.4	—	
Avg.		8.6	Avg.		11.4	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B203</u>			F ₀ _____		

Run/Sample No. <u>1-0-M3/MM10(A)4</u> Date <u>3/20/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator
							<u>SC6</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
0833	1045	8.6	19.9	—	11.3	—	
1	1055	8.5	20.0	—	11.5	—	
0936	1105	8.5	20.0	—	11.5	—	
Avg.		8.5	Avg.		11.4	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B100</u>			F ₀ _____		

METHOD 3 (ORSAT) FIELD DATA

Client Ogden
 Plant Name OMS LAKE
 City/State OKLAHOMA, FL
 Sampling Location UNIT No. 1 OUTLET

Job No. 10368
 Fuel Type MUNI WASTE

Run/Sample No. <u>1-0-mmwm/m3-5</u> Date <u>3/20/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1030	1145	8.3	19.5	—	11.2	—	
1	1155	8.3	19.5	—	11.2	—	
1133	1205	8.3	11.2	—	11.2	—	
Avg.		8.3	Avg.		11.2	—	
Orsat I.D. <u>2</u> Tedlar Bag I.D. <u>B200</u> F _o _____							SC6

Run/Sample No. <u>1-0-mm101A/m3-6</u> Date <u>3/20/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1200	1310	8.1	19.5	H	11.4	—	
1	1318	8.2	19.5	—	11.3	—	
1303	1330	8.2	19.5	—	11.3	—	
Avg.		8.2	Avg.		11.3	—	
Orsat I.D. <u>2</u> Tedlar Bag I.D. _____ F _o _____							SC6

Run/Sample No. <u>1-0-mm101A/m3-7</u> Date <u>3/20/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1333	1340 1440	8.3	19.7	—	11.4	—	
1	1350 1450	8.3	19.7	—	11.4	—	
1437	1350 1450	8.3	19.8	—	11.5	—	
Avg.		8.3	Avg.		11.4	—	
Orsat I.D. <u>2</u> Tedlar Bag I.D. <u>B139</u> F _o _____							SC6

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SAMPLING DATA - METHOD (S) MOD EPA 101A

CLIENT: DODEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORAHUMOKA, FL JOB NO.: 10388
 SAMPLE LOCATION: Unit 1 FF Outlet RUN NO.: 1-OMM101A-1
 BAR. PRESS., IN. HG: 29.6 STATIC PRESSURE, IN. H₂O: -17 DATE: 3/19/98
 LEAK ✓ VAC., IN. HG: 15 5 RUN TIME: 1010 - 1115
 LEAK RATE, CFM: 0.004 0.000 TEST PERSONS: WJ

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS			NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@		XAD	WT.		
PITOT	✓	✓	<u>2107</u>	<u>0.9757</u>	<u>1.787</u>					
TC	✓	✓	PITOT ID <u>14</u>	Cp <u>0.84</u>	METER TEMP. <u>90</u>		NA	NA		
NOZZLE	✓	✓	TC READOUT <u>Notech</u>	TC <u>17</u>	EST. % H ₂ O <u>17</u>					
ORSAT	✓	NA	NOZZLE NO. <u>GIN 284</u>	DIA. <u>0.218</u>	"C" FACTOR <u>0.755</u>					
			SAMPLE BOX <u>64</u>	REAGNT. <u>C14/206</u>	STACK TEMP. <u>280</u>					
			UMBILICAL <u>UAS</u>		REF DELTA-P <u>1.450</u>					
			ORSAT PUMP <u>ORI</u>	BAG <u>139</u>	"K" FACTOR <u>1.268</u>					

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			<u>85% Bay</u>

	PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	A-8	0	666.538	1.30	76	277	1.62	1.616	3	242	66	
2	7	25	668.535	1.40	77	278	1.74	1.738	3	241	59	
3	6	50	670.390	1.30	77	279	1.61	1.612	3	242	59	
	5	75	672.176	1.15	79	279	1.43	1.431	3	245	60	
	4	100	673.873	1.10	80	277	1.38	1.376	3	243	61	
6	3	125	675.525	1.05	81	277	1.32	1.316	3	243	62	
7	2	150	677.155	0.93	82	274	1.17	1.173	3	243	63	
8	1	175	678.67	0.72	83	265	0.92	0.921	3	246	64	
9	B-8	200	680.117	1.10	82	269	1.40	1.398	3	241	65	
10	7	225	681.865	1.05	85	273	1.33	1.333	3	246	63	
11	6	250	683.510	1.05	86	273	1.34	1.336	3	245	64	
12	5	275	685.152	1.05	87	273	1.34	1.338	3	247	64	
13	4	300	686.788	1.10	88	272	1.41	1.407	3	247	64	
14	3	325	688.51	1.20	89	272	1.54	1.537	3	247	63	
15	2	350	690.240	1.10	90	272	1.41	1.411	3	246	63	
16	1	375	691.984	0.87	90	268	1.12	1.122	3	247	64	
17	C-8	400	693.55	1.25	89	275	1.61	1.606	3	248	65	
18	7	425	695.410	1.20	92	271	1.55	1.546	3	247	64	
19	6	450	697.175	1.20	92	270	1.55	1.549	3	247	64	
20	5	475	698.955	1.15	93	268	1.49	1.491	3	249	65	
21	4	500	700.710	1.15	93	267	1.49	1.493	3	248	65	
22	3	525	702.465	1.10	93	268	1.43	1.426	3	245	65	
23	2	550	704.155	0.73	93	268	0.98	0.98	3	247	65	
	1	575	705.630	0.77	93	265	1.01	1.011	3	248	66	
END		600	707.157									

FINAL

REVIEWER WJ

60 40.619 1.0769 86.3 271.4 1.3821

SAMPLING DATA - METHOD (S) ^{mo} EPA 101A

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, OK JOB NO.: 10388
 SAMPLE LOCATION: Unit 1 FF Outlet RUN NO.: 1-0-MM161A-2
 BAR. PRESS., IN. HG: 29.6 STATIC PRESSURE, IN. H₂O: -17 DATE: 3/19/98
 LEAK ✓ VAC., IN. HG: 10 5 RUN TIME: 1355 - 1439
 LEAK RATE, CFM: 0.002 0.000 TEST PERSONS: WAT

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA HQ	XAD	WT.				
PITOT	✓	✓	<u>2107</u>	<u>0.9757</u>	<u>1.787</u>	<u>NA</u>	<u>NA</u>				
TC	✓	✓	PITOT ID <u>PT05</u>	Cp <u>0.84</u>	METER TEMP. <u>90</u>						
NOZZLE	✓	✓	TC READOUT <u>Nutek</u>	TC <u>49</u>	EST. % H ₂ O <u>17</u>						
ORSAT	✓	NA	NOZZLE NO. <u>G4254</u>	DIA. <u>0.216</u>	"C" FACTOR <u>0.755</u>						
			SAMPLE BOX <u>30</u>	REAGNT. <u>C14/200</u>	STACK TEMP. <u>280</u>						
			UMBILICAL <u>U95</u>		REF DELTA-P <u>1.005</u>						
			ORSAT PUMP <u>0R1</u>	BAG <u>B203</u>	"K" FACTOR <u>1.222</u>						

LEAK CHECKS	B E	B E	B E	B E	FYRITES	% O ₂	% CO ₂
							<u>8.5% Bal</u>

	PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	A-8	0	707.400	1.40	78	269	1.70	1.702	3	246	65	
2	7	2.5	709.415	1.30	79	271	1.58	1.576	3	239	62	
3	6R	5.0	711.168	1.25	79	271	1.52	1.516	3	236	63	
4	5R	7.5	712.915	1.15	80	271	1.40	1.398	3	248	64	
5	4R	10.0	714.610	1.06	81	269	1.29	1.274	3	242	64	
6	3R	12.5	716.232	0.96	81	269	1.17	1.173	3	241	64	
7	2R	15.0	717.75	0.88	82	269	1.08	1.077	3	237	66	
8	1R	17.5	719.265	0.69	83	259	0.86	0.86	3	244	66	
9	B-8	20.0	720.667	1.15	82	269	1.41	1.409	3	243	66	
10	B7R	22.5	722.400	1.05	83	270	1.29	1.285	3	236	65	
11	6R	25.0	724.022	0.97	84	270	1.19	1.190	3	243	64	
12	5R	27.5	725.570	0.95	84	270	1.17	1.166	3	235	64	
13	4R	30.0	727.110	0.99	84	270	1.22	1.25	3	246	65	
14	3R	32.5	728.692	1.05	84	269	1.29	1.290	3	245	64	
15	2R	35.0	730.360	0.94	84	267	1.16	1.158	3	244	65	
16	1R	37.5	731.875	0.71	85	260	0.89	0.885	3	242	65	
17	C8	40.0	733.288	1.30	83	268	1.60	1.598	3	245	65	
18	C7R	42.5	735.150	1.20	85	269	1.48	1.476	3	240	63	
19	6R	45.0	736.875	1.20	86	270	1.48	1.477	3	242	64	
20	5R	47.5	738.595	1.15	87	269	1.42	1.420	3	239	64	
21	4R	50.0	740.320	1.05	87	269	1.30	1.296	3	237	65	
22	3R	52.5	741.945	0.95	87	267	1.18	1.177	3	239	65	
23	2R	55.0	743.500	0.92	87	265	1.14	1.143	3	241	66	
24	1R	57.5	745.040	0.75	86	260	0.94	0.937	3	211	66	
25	-8	60.0	746.500									

FINAL 60 39.100 1.0343 83.4 2679 1.2817 REVIEWER [Signature]

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SAMPLING DATA - METHOD (S) _____

Page 1 of 1

CLIENT: OGDEN ENERGY GROUP, Inc PLANT: OGDEN MARTIN SYSTEMS OF LAKE, Inc
 CITY/STATE: OKLAHOMA, FL JOB NO.: 10328
 SAMPLE LOCATION: Unit 1 - FF Outlet RUN NO.: 1-0-MM101A-4
 BAR. PRESS., IN. HG: 29.5 STATIC PRESSURE, IN. H₂O: -17 DATE: 3/20/98
 LEAK ✓ VAC., IN. HG: 10 5 RUN TIME: 0833 - 0936
 LEAK RATE, CFM: 0.000 0.000 TEST PERSONS: WAS

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX		Y	DELTA H@			XAD	WT.	
PITOT	✓		PITOT ID	<u>14</u>	Cp	<u>0.84</u>	METER TEMP.	<u>85</u>	NA	NA	
TC	✓		TC READOUT	<u>Nutech</u>	TC	<u>17</u>	EST. % H ₂ O	<u>17</u>			
NOZZLE	✓		NOZZLE NO.	<u>GN297</u>	DIA	<u>0.218</u>	"C" FACTOR	<u>0.746</u>			
ORSAT	✓	NA	SAMPLE BOX	<u>64</u>	REAGNT.	<u>611/267</u>	STACK TEMP.	<u>280</u>			
			UMBILICAL	<u>U96</u>			REF DELTA-P	<u>1.464</u>			
			ORSAT PUMP	<u>OR1</u>	BAG	<u>3100</u>	"K" FACTOR	<u>1.257</u>			

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			<u>8% Bag</u>

	PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	A-8	0	750.7	1.20	75	269	1.57	1.505	3	243	62	
2	7	2.5	752.615	1.15	76	269	1.44	1.443	3	243	61	
3	6	5.0	754.288	1.20	76	271	1.20	1.502	3	243	63	
4	5	7.5	756.038	1.10	77	271	1.38	1.371	3	249	64	
5	4	10.0	757.69	1.00	78	272	1.26	1.255	3	242	65	
6	3	12.5	759.290	0.95	78	272	1.19	1.192	3	243	63	
7	2	15.0	760.845	0.89	79	270	1.12	1.122	3	243	63	
8	1	17.5	762.350	0.67	80	261	0.86	0.857	3	241	63	
9	B-8	20.0	763.750	0.94	79	268	1.19	1.190	3	244	65	
10	7	22.5	765.350	0.85	80	268	1.08	1.077	3	241	64	
11	6	25.0	766.835	0.85	80	267	1.08	1.079	3	244	65	
12	5	27.5	768.326	0.93	81	268	1.18	1.181	3	245	65	
13	4	30.0	769.870	1.00	81	270	1.27	1.276	3	250	66	
14	3	32.5	771.484	1.10	82	271	1.39	1.393	3	257	62	
15	2	35.0	773.155	1.05	81	272	1.33	1.325	3	250	62	
16	1	37.5	774.798	0.81	82	262	1.04	1.038	3	247	62	
17	C-8	40.0	776.34	1.10	80	264	1.40	1.402	3	258	66	
18	7	42.5	778.065	1.10	82	270	1.39	1.394	3	244	64	
19	6	45.0	779.753	1.05	82	268	1.34	1.335	3	240	65	
20	5	47.5	781.415	0.97	82	266	1.24	1.236	3	250	63	
21	4	50.0	783.012	1.08	83	268	1.38	1.376	3	250	64	
22	3	52.5	784.675	0.99	83	268	1.26	1.261	3	244	64	
23	2	55.0	786.288	1.00	83	269	1.27	1.272	3	243	65	
24	1	57.5	787.915	0.76	83	261	0.90	0.900	3	245	66	
25	END	60.0	789.31									

FINAL

REVIEWER _____

60 38.61 0.9816 80.1 268.1 1.250

SAMPLING DATA - METHOD (S)

CLIENT: OGDEN ENERGY GROUP, INC PLANT: OGDEN MARTIN SYSTEMS OF LAKE, INC
 CITY/STATE: OMAHA, NE JOB NO.: 10388
 SAMPLE LOCATION: Unit 1 - FF Outlet RUN NO.: 1-0-MMU1A-5
 BAR. PRESS., IN. HG: 29.5 STATIC PRESSURE, IN. H₂O: -17 DATE: 3/20/98
 LEAK ✓ VAC., IN. HG: 10 5 RUN TIME: 1030 - 1133
 LEAK RATE, CFM: 0.000 0.000 TEST PERSONS: WAT

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@				XAD	WT.	
PITOT	✓	✓	<u>2107</u>	<u>0.9707</u>	<u>1.787</u>				<u>NA</u>	<u>NA</u>	
TC	✓	✓	<u>15</u>	<u>0.84</u>	<u>80</u>						
NOZZLE	✓	✓	<u>TC READOUT</u>	<u>49</u>	<u>17</u>						
ORSAT	✓	NA	<u>NOZZLE NO. GN294</u>	<u>0.217</u>	<u>0.741</u>						
			<u>SAMPLE BOX 30</u>	<u>REAGNT. 611/207</u>	<u>270</u>						
			<u>UMBILICAL 095</u>		<u>1.485</u>						
			<u>ORSAT PUMP OR-1</u>	<u>BAG 3200</u>	<u>1.239</u>						

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			<u>8.5% O₂</u>

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	A-8	0	789.45	1.36	80	1.57	1.573	3	245	66	
2	7	2.5	791.81	1.25	82	290	1.57	1.573	3	246	65
3	6	5.0	793.08	1.50	82	291	1.81	1.814	3	242	65
4	5	7.5	794.977	1.35	82	291	1.63	1.631	3	239	65
5	4	10.0	796.795	1.25	83	293	1.57	1.570	3	249	65
6	3	12.5	798.557	1.10	84	293	1.33	1.332	3	252	66
7	2	15.0	800.215	0.94	84	289	1.14	1.144	3	241	66
8	1	17.5	801.775	0.70	84	281	0.86	0.862	3	253	66
9	B-8	20.0	803.170	0.95	83	280	1.17	1.170	3	242	67
10	7	22.5	804.772	0.91	84	284	1.12	1.116	3	240	62
11	6	25.0	806.288	0.89	84	288	1.09	1.086	3	245	61
12	5	27.5	807.775	0.89	85	292	1.08	1.082	3	249	61
13	4	30.0	809.280	0.99	85	293	1.20	1.202	3	242	62
14	3	32.5	810.880	1.10	85	292	1.34	1.337	3	245	62
15	2	35.0	812.53	1.03	86	290	1.26	1.257	3	248	62
16	1	37.5	814.14	0.69	86	279	0.86	0.855	3	243	63
17	C-8	40.0	815.507	1.25	85	282	1.54	1.541	3	246	65
18	7	42.5	817.293	1.20	86	288	1.47	1.468	3	238	64
19	6	45.0	819.850	1.10	86	290	1.34	1.342	3	247	64
20	5	47.5	820.700	1.00	87	292	1.22	1.219	3	242	64
21	4	50.0	822.297	1.00	87	291	1.22	1.221	3	249	63
22	3	52.5	823.910	1.07	88	289	1.31	1.313	3	246	64
23	2	55.0	825.55	0.97	88	287	1.19	1.193	3	251	65
24	1	57.5	827.122	0.83	87	276	1.03	1.034	3	246	66
25	END	60.0	828.598								

FINAL

REVIEWER

60 39.148 1.0434 84.7 287.8 1.2838

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SAMPLING DATA - METHOD (S)

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, FC JOB NO.: 10388
 SAMPLE LOCATION: Unit 1 - PF Outlet RUN NO.: 1-0-mm10A-6
 BAR. PRESS., IN. HG: 29.5 STATIC PRESSURE, IN. H₂O: -17 DATE: 3/20/98
 LEAK ✓ VAC., IN. HG: 10 5 RUN TIME: 1200 - 1303
 LEAK RATE, CFM: 0.000 0.002 TEST PERSONS: WJ

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H ₂ O	DELTA H ₂ O		XAD	WT.		
PITOT	✓		<u>2107</u>	<u>0.9757</u>	<u>1.787</u>						
TC	✓		PITOT ID <u>14</u>	Cp <u>0.84</u>	METER TEMP. <u>85</u>			N/A	N/A		
NOZZLE	✓		TC READOUT <u>Nature</u>	TC <u>17</u>	EST. % H ₂ O <u>17</u>						
ORSAT	✓	NA	NOZZLE NO. <u>GNA97</u>	DIA. <u>0.218</u>	"C" FACTOR <u>0.748</u>						
			SAMPLE BOX <u>64</u>	REAGNT. <u>611/207</u>	STACK TEMP. <u>285</u>						
			UMBILICAL <u>U95</u>		REF DELTA-P <u>1.474</u>						
			ORSAT PUMP <u>OR-1</u>	BAG <u>B100</u>	"K" FACTOR <u>1.248</u>						

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			<u>75% Bag</u>

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-8	0	828.750	1.20	85	284	1.50	1.502	3	241	67	
2	7	25	830.595	1.25	86	294	1.55	1.545	3	250	66	
3	6	50	832.375	1.30	86	293	1.61	1.609	3	252	63	
	5	75	834.78	1.15	86	292	1.43	1.425	3	248	64	
	4	100	835.890	0.98	87	291	1.22	1.218	3	247	66	
6	3	125	837.470	0.88	87	290	1.10	1.096	3	246	66	
7	2	150	838.985	0.82	87	289	1.02	1.023	3	253	65	
8	1	175	840.455	0.66	87	279	0.84	0.835	3	248	66	
9	B-8	200	841.875	0.93	87	285	1.17	1.167	3	246	66	
10	7	225	843.495	0.91	87	292	1.13	1.131	3	246	65	
11	6	250	844.985	0.89	88	295	1.10	1.104	3	242	64	
12	5	275	846.510	0.93	88	296	1.15	1.152	3	246	64	
13	4	300	848.000	1.00	88	296	1.24	1.238	3	243	63	
14	3	325	849.600	1.15	89	294	1.43	1.430	3	249	63	
15	2	350	851.380	1.05	89	292	1.31	1.308	3	248	63	
16	1	375	853.035	0.87	89	278	1.11	1.105	3	247	63	
17	C-8	400	854.57	1.20	88	289	1.50	1.500	3	246	63	
18	7	425	856.335	1.15	89	291	1.44	1.425	3	243	68	
19	6	450	858.05	1.07	89	292	1.33	1.333	3	245	63	
20	5	475	859.705	1.15	89	292	1.43	1.433	3	248	63	
21	4	500	861.425	1.05	89	293	1.31	1.307	3	248	63	
22	3	525	863.065	1.15	89	292	1.43	1.434	3	250	65	
23	2	550	864.815	0.99	89	291	1.24	1.235	3	246	66	
	1	575	866.405	0.86	89	275	1.10	1.097	3	250	66	
	END	600	867.923									

FINAL 39

REVIEWER

60 39.173 1.0186 87.8 289.8 1.2708

SAMPLING DATA - METHOD (S)

CLIENT: DODEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORAHAMOKA, FL JOB NO.: 10388
 SAMPLE LOCATION: Unit 1 - FF Outlet RUN NO.: 1-0-mm101A-7
 BAR. PRESS., IN. HG: 295 STATIC PRESSURE, IN. H₂O: -17 DATE: 3/20/98
 LEAK ✓ VAC., IN. HG: 10 5 RUN TIME: 1332 - 1437
 LEAK RATE, CFM: 0.002 0.000 TEST PERSONS: WAJ

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	<u>2107</u>	Y	<u>0.9757</u>	DELTA H@	<u>1.787</u>		XAD	WT.
PITOT	✓	✓	PITOT ID	<u>15</u>	Cp	<u>0.84</u>	METER TEMP.	<u>85</u>		NA	NA
TC	✓	✓	TC READOUT	<u>Nutech</u>	TC	<u>49</u>	EST. % H ₂ O	<u>17</u>			
NOZZLE	✓	✓	NOZZLE NO.	<u>GN24</u>	DIA.	<u>0.217</u>	"C" FACTOR	<u>0.748</u>			
ORSAT	✓	NA	SAMPLE BOX	<u>30</u>	REAGNT.	<u>611/207</u>	STACK TEMP.	<u>290</u>			
			UMBILICAL	<u>V95</u>			REF DELTA-P	<u>1.512</u>			
			ORSAT PUMP	<u>DR-1</u>	BAG	<u>B189</u>	"K" FACTOR	<u>1.217</u>			

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			<u>7 % Bag</u>

PT. NO.	ELAPSED TIME, MINUTES	DCM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DCM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-8	0	868.500	1.30	85	287	1.59	1.591	3	241	66	
2	7	205	876.38	1.20	86	289	1.47	1.465	3	240	65	
3	6	5.0	872.172	1.15	87	290	1.405	1.405	3	239	62	
4	5	7.5	873.885	1.10	87	291	1.34	1.343	3	248	64	
5	4	100	875.540	0.97	88	292	1.19	1.185	3	237	64	
6	3	125	877.112	0.93	88	291	1.14	1.138	3	240	64	
7	2	15.0	878.662	0.84	88	291	1.03	1.028	3	240	64	
8	1	175	880.140	0.73	88	279	0.91	0.908	3	237	65	
9	B-8	200	881.63	0.92	87	285	1.13	1.134	3	246	66	
10	7	225	883.200	0.86	88	290	1.05	1.054	3	242	65	
11	6	250	884.675	0.86	88	292	1.05	1.051	3	239	64	
12	5	275	886.17	0.91	88	293	1.11	1.111	3	240	64	
13	4	300	887.670	0.99	88	293	1.21	1.208	3	242	64	
14	3	325	889.206	1.10	88	292	1.34	1.344	3	240	65	
15	2	350	890.95	1.05	88	292	1.28	1.283	3	238	66	
16	1	375	892.573	0.82	88	276	1.02	1.024	3	242	62	
17	C-8	400	894.150	1.25	86	286	1.54	1.535	3	239	61	
18	7	425	895.970	1.15	87	289	1.41	1.407	3	238	61	
19	6	450	897.120	1.10	87	290	1.35	1.345	3	239	62	
20	5	475	899.317	1.05	87	291	1.28	1.282	3	247	62	
21	4	500	900.925	1.08	87	291	1.32	1.319	3	243	63	
22	3	525	902.585	1.08	87	290	1.32	1.320	3	243	64	
23	2	55.0	904.23	0.93	86	284	1.14	1.144	3	244	64	
1	575	905.782	0.88	87	286		1.12	1.097	3	243	66	
BND	600	907.33										

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REVIEWER

60 38.83 1.003 87.3 288.3 1.2894

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SAMPLING DATA - METHOD (S) EPA 101A

CLIENT: DODEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, FC JOB NO.: 10388
 SAMPLE LOCATION: UNIT No. 1 OUTLET RUN NO.: 1-0-M26-1
 BAR. PRESS., IN. HG: 29.5 STATIC PRESSURE, IN. H₂O: 0.007 DATE: 3/20/98
 LEAK ✓ VAC., IN. HG: 18 S RUN TIME: 1402-1447
 LEAK RATE, CFM: 0.008 0.002 TEST PERSONS: SLC, WJS

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX		Y	DELTA HQ			XAD	WT.	
PITOT	NA	—	NA	NA	CP	NA	METER TEMP.	NA	NA	NA	
TC	NA	—	TC READOUT	NA	TC	NA	EST. % H ₂ O				
NOZZLE	NA	—	NOZZLE NO.	NA	DIA	NA	"C" FACTOR				
ORSAT	NA	NA	SAMPLE BOX	NA	REAGNT.		STACK TEMP.				
			UMBILICAL	NA			REF DELTA-P				
			ORSAT PUMP	NA	BAG	NA	"K" FACTOR				

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂		
	E	E	E	E		% CO ₂		

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	0	924.062	NA	77	NA	1.8	1.8	4	262	66	NA
2	5	926.71		77		1.8		4	254	68	
3	10	930.57		78		1.8		5	232	70	
	15	-		80		1.8		5	230	70	
	20	939.35		80		1.8		5	230	70	
6	25	943.		80		1.8		5	235	72	
7	30	947.		80		1.8		5	239	72	
8	35	951.49		80		1.8		5	244	72	
9	40	955.6		81		1.8		5	258	66	
10	45	959.615									
11											
12											
13											
14											
15											
16											
17											
18											
19											
20											
21											
22											
23											

FINAL _____ REVIEWER _____

45 35.553 NA 79.2 NA 1.8

APPENDIX C

FIELD DATA

2.0 UNIT NO. 2

a. INLET

METHOD 3 (ORSAT) FIELD DATA

Client ODDEN ENERGY

Job No. 10388

Plant Name DMS LAKE

Fuel Type MUNI WASTE

City/State OKAHUMPKA, FL

Sampling Location UNIT NO. 2 INLET ~~OUTLET~~

Run/Sample No. <u>2-I-M101A/M3-1</u> Date <u>3/18/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1616	1758	8.4	20.0	—	11.6	—	
1	1806	8.5	20.2	—	11.7	—	
1728	1818	8.4	20.1	—	11.7	—	
Avg.		8.4	Avg.		11.7	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B100</u>		F _o _____			

Run/Sample No. <u>2-I-M101A/M3-1</u> Date <u>3/18/98</u> Leak <input checked="" type="checkbox"/> OK? <input checked="" type="checkbox"/>							Operator <u>SCG</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1758	1944	8.2	19.6	—	11.4	—	
1	1950	8.2	19.6	—	11.4	—	
1912	1955	8.2	19.6	—	11.4	—	
Avg.		8.2	Avg.		11.4	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. _____		F _o _____			

Run/Sample No. _____ Date _____ Leak <input type="checkbox"/> OK? <input type="checkbox"/>							Operator _____
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
Avg.			Avg.				
Orsat I.D. _____		Tedlar Bag I.D. _____		F _o _____			

SAMPLING DATA - METHOD (S) 101A

CLIENT: ODDEN ENERGY GROUP PLANT: OMS LAKE 2-I-m101A-1
 CITY/STATE: ORAHUMPKA, FL JOB NO: 10388
 SAMPLE LOCATION: 2-I-m101A-1 RUN NO: 10388
 BAR. PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: -1.7 DATE: 3-18-98
 LEAK ✓ VAC., IN. HG: 0.000 0.001 RUN TIME: 1616 - 1728
 LEAK RATE, CFM: 15 11 TEST PERSONS: AS DB

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@		XAD	WT.			
PITOT	✓	✓	<u>2108</u>	<u>1.0138</u>	<u>1.712</u>						
TC	✓	✓	PITOT ID <u>017</u>	Cp <u>0.84</u>	METER TEMP. <u>90</u>						
NOZZLE	✓	✓	TC READOUT <u>2108</u>	TC <u>56</u>	EST. % H ₂ O <u>12</u>						
ORSAT	✓	NA	NOZZLE NO. <u>FN2010</u>	DIA. <u>0.356</u>	"C" FACTOR <u>0.825</u>						
			SAMPLE BOX <u>02</u>	REAGNT. <u>214</u>	STACK TEMP. <u>450</u>						
			UMBILICAL		REF DELTA-P <u>0.855</u>						
			ORSAT PUMP <u>0R2</u>	BAG <u>B100</u>	"K" FACTOR <u>2.52</u>						

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

PT. NO.	ELAPSED TIME, MINUTES	DCM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DCM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A 1	0	361.448	0.54	61	413	1.2	1.142	2	237	68	NA
2	2	2 1/2	363.57	0.62	61	424	1.35	1.351	2	233	68	
3	3	5	365.22	0.66	61	427	1.4	1.433	2	235	67	
4	4	7 1/2	366.84	0.67	62	429	1.45	1.454	3	240	68	
5	5	10	364.61	0.66	62	426	1.4	1.437	3	235	68	
6	6	12 1/2	370.32	0.71	63	426	1.55	1.545	3	238	67	
7	7	15	372.02	0.7	64	424	1.5	1.533	4	240	68	
8	8	17 1/2	373.7	0.69	65	423	1.5	1.525	4	236	69	
9	B 1	20	375.089	0.46	62	417	1	1.011	4	237	69	
10	2	22 1/2	376.93	0.54	64	422	1.2	1.186	5	239	69	
11	3	25	378.535	0.54	64	423	1.2	1.285	5.5	239	64	
12	4	27 1/2	380.78	0.61	64	423	1.35	1.390	6	240	63	
13	5	30	381.66	0.66	64	420	1.45	1.452	6	241	61	
14	6	32 1/2	383.2	0.66	64	420	1.45	1.552	6	241	61	
15	7	35	384.45	0.7	64	414	1.55	1.542	7	240	61	
16	8	37 1/2	386.7	0.72	64	421	1.6	1.582	7.5	240	61	
17	C 1	40	388.431	0.44	60	409	0.95	0.973	8	239	61	
18	2	42 1/2	389.8	0.59	61	421	1.3	1.291	8	238	61	
19	3	45	391.31	0.6	61	420	1.3	1.313	8	241	60	
20	4	47 1/2	392.9	0.59	61	421	1.3	1.290	9	240	61	
21	5	50	394.54	0.6	63	422	1.3	1.315	9	239	61	
22	6	52 1/2	396.205	0.64	62	424	1.4	1.397	9	250	61	
23	7	55	397.8	0.66	63	421	1.5	1.442	9	245	61	
8	57 1/2	399.48	0.71	63	420	1.55	1.551	10	251	61		
END	60	401.252										

FINAL

REVIEWER

60 39304 0.6180 82.7 421.5 1.36

CLIENT: ODDEN ENERGY PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, OK JOB NO.: 10388
 SAMPLE LOCATION: Inlet Unit 2 RUN NO.: 2-10-101A-1
 BAR. PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: -2.5 DATE: 3/8-98
 LEAK ✓ VAC., IN. HG: 15 RUN TIME: 1758-1912
 LEAK RATE, CFM: 0.005 TEST PERSONS: AG DB

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	Y	DELTA H@		XAD	WT.			
PITOT	✓	✓	2108	1.0138	1.72						
TC	✓	✓	PITOT ID DT3	Cp 0.84	METER TEMP. 90						
NOZZLE	✓	✓	TC READOUT 2108	TC 4/56	EST. % H ₂ O 12						
ORSAT	✓	NA	NOZZLE NO. 6N2006	DIA. 0.255	"C" FACTOR 0.828						
			SAMPLE BOX 08	REAGNT. 632/215	STACK TEMP. 450						
			UMBILICAL		REF DELTA-P 0.868						
			ORSAT PUMP OR2	BAG 13200	"K" FACTOR 2.119						

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	A-1	401.693	0.56	77	400	1.3	1.27	3	224	68	NA
2	2	403.2	0.56	78	432	1.2	1.184	4	224	65	
3	3	404.8	0.62	78	433	1.3	1.309	4	230	64	
4	4	406.505	0.65	79	432	1.4	1.376	4	230	60	
5	5	408.16	0.66	80	430	1.4	1.403	5	232	60	
6	6	409.79	0.68	80	430	1.45	1.446	6	230	62	
7	7	411.5	0.7	81	432	1.5	1.504	6	233	63	
8	8	413.12	0.7	81	429	1.5	1.492	6	232	63	
9	B-1	414.819	0.5	77	410	1.1	1.081	6	233	64	
10	2	416.41	0.55	79	419	1.2	1.188	6	242	65	
11	3	417.835	0.57	78	426	1.2	1.203	6	233	62	
12	4	419.398	0.54	79	424	1.15	1.154	7	227	54	
13	5	420.88	0.63	80	426	1.35	1.346	7	237	54	
14	6	422.454	0.64	80	427	1.5	1.472	8	237	55	
15	7	424.15	0.69	80	426	1.5	1.473	8	237	55	
16	8	425.805	0.66	81	424	1.45	1.458	9	237	54	
17	C-1	427.448	0.61	78	414	1.3	1.315	9	242	54	
18	2	429.14	0.66	80	424	1.4	1.403	9	239	55	
19	3	430.74	0.65	80	424	1.4	1.385	9	239	55	
20	4	432.41	0.59	80	427	1.25	1.259	10	235	55	
21	5	433.97	0.59	80	427	1.25	1.259	11	238	58	
22	6	435.521	0.62	80	424	1.3	1.327	11	240	58	
23	7	437.19	0.63	80	426	1.35	1.346	12	239	58	
	8	438.83	0.67	80	426	1.45	1.431	13	239	54	
	END	440.445									

FINAL

REVIEWER

100 38.825 0.1650 79.4 424.8 1.34

C 23

AirKinetics, Inc.

APPENDIX C

FIELD DATA

2.0 UNIT NO. 2

b. STACK

METHOD 3 (ORSAT) FIELD DATA

Client OGDEN ENERGY
 Plant Name DMS LAKE
 City/State OKAUCHUKA, FL
 Sampling Location UNIT NO. 2 OUTLET

Job No. 10388
 Fuel Type MUNI WASTE

Run/Sample No. <u>2-0-M101A/M3-1</u> Date <u>3/18/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator <u>SC6</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1616	1736	8.2	20.2	—	12.0	—	
1	1740	8.4	20.5	—	12.1	—	
1719	1750	8.3	20.4	—	12.0	—	
Avg.		8.3	Avg.		12.0	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B139</u>		F ₀ _____			

Run/Sample No. <u>2-0-M101A/M3-1</u> Date <u>3/18/98</u> Leak v OK? <input checked="" type="checkbox"/>							Operator <u>SC6</u>
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
1803	1918	8.3	20.3	—	12.0	—	
1	1926	8.3	20.3	—	12.0	—	
1912	1936	8.3	20.3	—	12.0	—	
Avg.		8.3	Avg.		12.0	—	
Orsat I.D. <u>2</u>		Tedlar Bag I.D. <u>B148</u>		F ₀ _____			

Run/Sample No. _____ Date _____ Leak v OK? _____							Operator _____
Time of Sample Collection	Time of Analysis	CO ₂ Reading (A)	O ₂ Reading (B)	CO Reading (C)	% O ₂ (B-A)	% CO (C-B)	Concurrent Runs to Share Orsat Data
Avg.			Avg.				
Orsat I.D. _____		Tedlar Bag I.D. _____		F ₀ _____			

CLIENT: DODEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: OKLAHOMA, OK JOB NO.: 10388
 SAMPLE LOCATION: Unit 2 FF Outlet RUN NO.: 2-09101A-1
 BAR PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: -17.0 DATE: 3/18/98
 LEAK ✓ VAC., IN. HG: 16 3 RUN TIME: 1616 - 1719
 LEAK RATE, CFM: 0.004 0.002 TEST PERSONS: WAS

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS		NOMOGRAPH		FILTER	TARE
	PRE	POST	METER BOX		DELTA H ₂ O		XAD	WT.
PITOT	✓	✓	2107	Y 0.9757	1.787		NA	NA
TC	✓	✓	PITOT ID 13	Cp 0.84	METER TEMP. 96			
NOZZLE	✓	✓	TC READOUT <u>Nutec</u>	TC 7	EST. % H ₂ O 17			
ORSAT	✓	NA	NOZZLE NO. <u>GN296</u>	DIA 0.219	"C" FACTOR 0.733			
			SAMPLE BOX 73	REAGNT. <u>M147</u>	STACK TEMP. 280			
			UNIBILICAL <u>US5</u>		REF DELTA-P 1.428			
			ORSAT PUMP <u>OR1</u>	BAG <u>B139 A</u>	"K" FACTOR 1.289			

LEAK CHECKS	B	B	B	B	FYRITES	% O ₂	% CO ₂
	E	E	E	E			
							<u>7.6% Avg</u>

	PT. NO.	ELAPSED TIME, MINUTES	DCM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DCM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT
1	A-8	0	591.900	1.20	88	280	1.54	1.543	2	247	63	NA
2	7	2.5	593.855	1.20	88	283	1.54	1.535	2	243	62	
3	6	5.0	595.635	1.05	89	286	1.34	1.340	2	238	62	
	5	7.5	597.288	0.99	89	287	1.26	1.262	2	251	63	
	4	10.0	598.89	0.89	91	289	1.14	1.136	2	245	63	
6	3	12.5	600.420	0.78	90	288	1.06	0.995	2	242	64	
7	2	15.0	601.885	0.61	91	279	0.79	0.776	2	250	65	
8	1	17.5	603.210	0.46	91	270	0.52	0.524	2	248	65	
9	B-8	20.0	604.34	0.99	91	278	1.29	1.285	2	238	63	
10	7	22.5	605.925	0.95	92	286	1.22	1.220	2	241	62	
11	6	25.5	607.520	0.86	92	287	1.10	1.103	2	242	62	
12	5	27.5	609.037	0.84	93	286	1.08	1.081	2	247	63	
13	4	30.0	610.535	0.84	93	285	1.08	1.082	2	244	64	
14	3	32.5	612.035	0.82	92	284	1.06	1.056	2	244	64	
15	2	35.0	613.540	0.72	93	284	0.93	0.929	2	248	64	
16	1	37.5	614.960	0.50	92	269	0.66	0.656	2	230	63	
17	C-8	40.0	616.320	1.10	89	270	1.42	1.422	2	243	64	
18	7	42.5	618.130	1.05	90	285	1.34	1.344	2	250	64	
19	6	45.0	619.660	1.10	89	284	1.41	1.408	2	249	64	
20	5	47.5	621.360	1.08	89	284	1.38	1.382	2	245	65	
21	4	50.0	623.042	0.95	89	285	1.21	1.214	2	251	64	
22	3	53.5	624.625	0.78	90	285	1.00	0.999	2	247	64	
23	2	55.0	626.120	0.78	89	283	1.00	1.001	2	248	64	
	1	57.5	627.63	0.67	89	269	0.88	0.877	2	249	65	
	END	60.0	629.205									
	FINAL		37.115									

REVIEWER SLC

60 37.115 0.8682 90.4 282.2 E.1329

SAMPLING DATA - METHOD (S) Mod EPA 101A

CLIENT: DODEN ENERGY GROUP PLANT: OMS LAKE
 CITY/STATE: ORAHAMPA, FC JOB NO.: 10388
 SAMPLE LOCATION: Unit 2 FF Outlet RUN NO.: 2-0170A-1
 BAR. PRESS., IN. HG: 29.8 STATIC PRESSURE, IN. H₂O: -17.0 DATE: 3/18/98
 LEAK ✓ VAC., IN. HG: 11 4 4 RUN TIME: 1803 - 1912
 LEAK RATE, CFM: 0.000 0.000 0.000 TEST PERSONS: WAT

EQUIPMENT CHECKS			EQUIPMENT I.D. NUMBERS				NOMOGRAPH			FILTER	TARE
	PRE	POST	METER BOX	<u>2107</u>	Y	<u>0.9757</u>	DELTA H@	<u>1.787</u>		XAD	WT.
PITOT	✓	✓	PITOT ID	<u>PT15</u>	Cp	<u>0.84</u>	METER TEMP.	<u>90</u>		NA	NA
TC	✓	✓	TC READOUT	<u>Nurech</u>	TC	<u>49</u>	EST. % H ₂ O	<u>17</u>			
NOZZLE	✓	✓	NOZZLE NO.	<u>6N254</u>	DIA.	<u>0.216</u>	"C" FACTOR	<u>0.753</u>			
ORSAT	✓	NA	SAMPLE BOX	<u>30</u>	REAGNT.	<u>C14820</u>	STACK TEMP.	<u>280</u>			
			UMBILICAL	<u>U95</u>			REF DELTA-P	<u>1.589</u>			
			ORSAT PUMP	<u>OR1</u>	BAG	<u>8148B</u>	"K" FACTOR	<u>1.219</u>			

LEAK CHECKS	B	E	B	E	B	E	FYRITES	% O ₂	% CO ₂
	<u>653.63</u>								
	<u>653.66</u>							<u>7% Bk</u>	

PT. NO.	ELAPSED TIME, MINUTES	DGM READING, CUBIC FEET	PITOT READING, IN. H ₂ O	DGM TEMP, °F	STACK TEMP, °F	ORIFICE SETTING, IN. H ₂ O		GAUGE VACUUM, IN. HG.	GAS TEMPERATURES, °F			
						ACTUAL	IDEAL		FILTER BOX	IMPINGER EXIT	PROBE OR COND. EXIT	
1	A-8	0	629.150	1.26	84	282	1.45	1.446	3	237	64	
2	7	25	631.045	1.20	85	288	1.44	1.435	3	241	63	
3	6	50	632.755	1.10	85	287	1.32	1.317	3	238	62	
4	5	75	634.407	1.05	86	288	1.26	1.258	3	242	60	
5	4	100	635.990	0.91	86	287	1.09	1.092	3	236	61	
6	3	125	637.525	0.89	86	286	1.07	1.070	3	239	63	
7	2	150	638.975	0.74	86	281	0.80	0.806	3	245	62	
8	1	175	640.340	0.54	87	267	0.67	0.668	2	240	62	
9	B-8	200	641.545	1.10	85	279	1.33	1.334	3	243	64	
10	7	225	643.25	0.88	87	286	1.06	1.059	3	241	63	
11	6	250	644.755	0.88	87	286	1.06	1.060	3	243	62	
12	5	275	646.24	0.90	87	285	1.09	1.086	3	235	62	
13	4	300	647.77	0.91	87	285	1.10	1.098	3	245	61	
14	3	325	649.295	0.95	87	284	1.15	1.147	3	242	62	
15	2	350	650.820	0.87	88	284	1.05	1.053	3	244	63	
16	1	375	652.325	0.57	88	269	0.70	0.704	3	242	64	
17	C-8	400	653.63	1.25	85	282	1.51	1.570	3	236	65	
18	7	425	655.585	1.20	86	286	1.44	1.441	3	238	63	
19	6	450	657.295	1.15	87	286	1.38	1.384	3	241	63	
20	5	475	658.975	1.10	87	286	1.32	1.324	3	242	64	
21	4	500	660.615	1.05	88	286	1.27	1.266	3	244	65	
22	3	525	662.190	0.93	87	286	1.12	1.126	3	245	65	
23	2	550	663.740	0.66	87	268	0.82	0.80	3	241	66	
24	1	575	665.06	0.60	87	262	0.75	0.747	3	245	66	
25	END	600	666.375									

FINAL

REVIEWER SLC

60 37.195 0.9310 865 281.7 1.1376

APPENDIX D

ANALYTICAL DATA

1.0 MOISTURE ANALYTICAL SHEETS

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10388
 City / State OKAHUMPKA, FL Sampling Loc. #2 SDA Inlet

Run Number	<u>2-I-mm101A-1</u>	<u>1-I-mm101A-1</u>	<u>1-I-mm101A-2</u>
Sampling Date	<u>3/16/98</u>	<u>3/19/98</u>	<u>3/19/98</u>
Analysis Date	<u>"</u>	<u>"</u>	<u>"</u>
Analyst	<u>HDP</u>	<u>HDP</u>	<u>HDP</u>

<u>Reagent 1 (KCl Imp 1 + 2)</u>			
Final Weight, g	<u>369.9</u>	<u>387.7</u>	<u>357.5</u>
Tared Weight, g	<u>255.6</u>	<u>256.5</u>	<u>258.9</u>
Water Catch, g	<u>114.3</u>	<u>131.2</u>	<u>98.6</u>
<u>Reagent 2 (KCl Imp 3)</u>			
Final Weight, g	<u>144.3</u>	<u>149.9</u>	<u>145.5</u>
Tared Weight, g	<u>141.8</u>	<u>141.8 144.2</u>	<u>142.5</u>
Water Catch, g	<u>2.5</u>	<u>5.7</u>	<u>3.0</u>
<u>Reagent 3 (KMnO4)</u>			
Final Weight, g	<u>602.2</u>	<u>605.3</u>	<u>600.4</u>
Tared Weight, g	<u>600.0</u>	<u>605.3</u>	<u>600.4</u>
Water Catch, g	<u>2.2</u>	<u>0.0</u>	<u>0.0</u>
CONDENSED WATER, g	<u>119.0</u>	<u>136.9</u>	<u>111.6 101.6 (SF)</u>
<u>Silica Gel</u>			
Final Weight, g	<u>209.8</u>	<u>211.4</u>	<u>207.1</u>
Tared Weight, g	<u>200.0</u>	<u>200.0</u>	<u>200.0</u>
Water Catch, g	<u>9.8</u>	<u>11.4</u>	<u>7.1</u>
TOTAL WATER COLLECTED, g	<u>128.8</u> ✓	<u>148.3</u> ✓	<u>108.7 (SF)</u> <u>118.7</u>

Balance No. 3 Type (✓) Triple Beam Electronic Reagent Box 215
 Balance located in stable, draft-free area (✓)? Yes No (If "No," explain below.)

Comments balance in lab trailer D 2

FIELD SAMPLE RECOVERY QUALITY CONTROL

Box No. 215 Assembly Date 3/14/98 Assembled By G. MATA

Client OGDEN MARTIN SYSTEMS Job No. 10388

Plant OMS - LAKE City/State OKAHUMPKA, FL

Sampling Location #1 SDA Inlet Method mod. 101A

Individual Tare of Reagent ~~150~~ 200 (ml) (gm) of KCl

Individual Tare of Reagent 100 (ml) (gm) of KCl

Individual Tare of Reagent 200 (ml) (gm) of K₂MnO₄

Individual Tare of Silca Gel 200 gm

Other (specify)

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
<u>1-I-mm101A-1</u>	<u>3/19/98</u>	<u>NA</u>	<u>NA</u>	<u>Y</u>	<u>HD</u>	<u>3/19/98</u>	<u>20</u>	<u>Y</u>	<u>HD</u>
				Filter Appearance* <u>dirty</u> Reagent Appearance* <u>ok</u>					
<u>1-I-mm101A-2</u>	<u>3/19/98</u>	<u>NA</u>	<u>NA</u>	<u>Y</u>	<u>HD</u>	<u>3/19/98</u>	<u>25</u>	<u>Y</u>	<u>HD</u>
				Filter Appearance* <u>same</u> Reagent Appearance* <u>ok</u>					
<u>2-I-mm101A-3</u>									
				Filter Appearance* Reagent Appearance* 					
				Filter Appearance* Reagent Appearance* 					

ABORTED

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS

RECORD OF CUSTODY, CONTAINER No. 215

Client OGDEN MARTIN SYSTEMS

Job No. 10388

Plant Name OMS - LAKE

City/State OKLAHOMA, FL

Sampling Method (s) #1 SDA Inlet (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify)

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002615	3/14/98	0747	S	<i>[Signature]</i>	change train
	3/18/98	1600	B	<i>[Signature]</i>	
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Scaled By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact?***		
_____	_____	_____	Yes	No	N/A
Signature	Date	Time			

As Applicable:
All liquid levels at mark (✓) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____

CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10388
 City/State OKAHUMPKA, FL Sampling Loc. #1 SDA Inlet

Run Number	<u>1-I-MM101A-4</u>	<u>1-I-MM101A-5</u>	<u>1-I-MM101A-6</u>
Sampling Date	<u>3/20/98</u>	<u>3/20/98</u>	<u>3/20/98</u>
Analysis Date	<u>3/20/98</u>	<u>3/20/98</u>	<u>3/20/98</u>
Analyst	<u>HTD</u>	<u>HTD</u>	<u>HTD</u>

<u>Reagent 1 (KCl Imp 1+2)</u>			
Final Weight, g	<u>394.0</u>	<u>378.2</u>	<u>396.9</u>
Tared Weight, g	<u>259.0</u>	<u>253.7</u>	<u>255.9</u>
Water Catch, g	<u>135.0</u>	<u>124.5</u>	<u>141.0</u>
<u>Reagent 2 (KCl Imp 3)</u>			
Final Weight, g	<u>151.2</u>	<u>150.7</u>	<u>148.9</u>
Tared Weight, g	<u>143.0</u>	<u>139.7</u>	<u>141.1</u>
Water Catch, g	<u>8.2</u>	<u>11.0</u>	<u>7.8</u>
<u>Reagent 3 (KMnO4 / H2SO4)</u>			
Final Weight, g	<u>599.4</u>	<u>600.2</u>	<u>607.1</u>
Tared Weight, g	<u>597.7</u>	<u>600.2</u>	<u>606.0</u>
Water Catch, g	<u>1.7</u>	<u>0.0</u>	<u>1.1</u>
CONDENSED WATER, g	<u>144.9</u>	<u>135.5</u>	<u>149.9</u>
<u>Silica Gel</u>			
Final Weight, g	<u>213.2</u>	<u>209.6</u>	<u>211.8</u>
Tared Weight, g	<u>200.0</u>	<u>200.0</u>	<u>200.0</u>
Water Catch, g	<u>13.2</u>	<u>9.6</u>	<u>11.8</u>
TOTAL WATER COLLECTED, g	<u>158.1</u>	<u>145.1</u>	<u>161.7</u>

Balance No. 3 Type (✓) Triple Beam Electronic Reagent Box 205
 Balance located in stable, draft-free area (✓)? Yes No (If "No," explain below)

Comments balance in lab trailer

Box No. 205 Assembly Date 3/14/98 Assembled By G. MATA
 Client OGDEN MARTIN SYSTEMS Job No. 10388
 Plant OMS - LAKE City/State OKAHUMPKA, FL
 Sampling Location #1 SDA Inlet Method 101A

Individual Tare of Reagent 200 (ml) (gm) of 0.1 M KCl
 Individual Tare of Reagent 100 (ml) (gm) of "
 Individual Tare of Reagent 200 (ml) (gm) of 4% KMnO4 / 10% H2SO4
 Individual Tare of Silca Gel 200 gm

Other (specify)

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
1-I-MM101A-4	3/20	NA	NA	Y	HD	3/20	20	Y	HD
1-I-MM101A-5	3/20			Y	HD	3/20	25	Y	HD
1-I-MM101A-6	3/20			Y	HD	3/20	30	Y	HD
1-I-MM101A-7	3/20	✓	✓	Y	HD	3/20	25	Y	HD

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS _____

RECORD OF CUSTODY, CONTAINER No. 205

Client OGDEN MARTIN SYSTEMS

Job No. 10388

Plant Name OMS - LAKE

City/State OKAHUMKA, FL

Sampling Method (s) #1 SDA Inlet (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002780	3/14/98	0813	S	<i>[Signature]</i>	
	3/18/98	1000	B	<i>[Signature]</i>	<i>change team's</i>
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact?**	
_____	_____	_____	Yes ___	No ___ N/A ___
Signature	Date	Time		

As Applicable:
All liquid levels at mark (✓) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____
CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10388
 City/State OKAHUMPKA, FL Sampling Loc. #1 + #2 FF Outlet

Run Number	<u>2-0-mm101A-1</u>	<u>1-0-mm101A-1</u>	<u>1-0-mm101A-2</u>
Sampling Date	<u>3/18/98</u>	<u>3/19/98</u>	<u>3/19/98</u>
Analysis Date	"	"	"
Analyst	<u>HTD</u>	<u>HTD</u>	<u>HTD</u>

<u>Reagent 1 (KCl Imp 1+2)</u>			
Final Weight, g	<u>379.2</u>	<u>430.0</u>	<u>415.2</u>
Tared Weight, g	<u>258.2</u>	<u>237.0</u>	<u>268.7</u>
Water Catch, g	<u>121.0</u>	<u>173.0</u>	<u>146.5</u>
<u>Reagent 2 (KCl Imp 3)</u>			
Final Weight, g	<u>143.2</u>	<u>141.5</u>	<u>150.0</u>
Tared Weight, g	<u>142.3</u>	<u>141.5</u>	<u>148.4</u>
Water Catch, g	<u>0.9</u>	<u>0.0</u>	<u>1.6</u>
<u>Reagent 3 (KMnO4)</u>			
Final Weight, g			
Tared Weight, g	<u>600.8</u>	<u>600.4</u>	<u>603.8</u>
Water Catch, g	<u>600.6</u> <u>0.2</u>	<u>600.3</u>	<u>603.6</u> <u>0.2</u>
CONDENSED WATER, g	<u>122.1</u>	<u>0.1</u> <u>173.1</u>	<u>148.3</u>
<u>Silica Gel</u>			
Final Weight, g	<u>210.7</u>	<u>208.2</u>	<u>207.3</u>
Tared Weight, g	<u>200.0</u>	<u>200.0</u>	<u>200.0</u>
Water Catch, g	<u>10.7</u>	<u>8.2</u>	<u>7.3</u>
TOTAL WATER COLLECTED, g	<u>132.8</u> ✓	<u>181.3</u> ✓	<u>155.6</u> ✓

Balance No. 3 Type (✓) Triple Beam Electronic Reagent Box 206
 Balance located in stable, draft-free area (✓)? Yes No (If "No," explain below.)

Comments balance in lab trailer D 8

FIELD SAMPLE RECOVERY QUALITY CONTROL

Box No. 206 Assembly Date 3/14/98 Assembled By G. MATA
 Client OGDEN MARTIN SYSTEMS Job No. 10388
 Plant OMS - LAKE City / State OKAHUMPKA, FL
 Sampling Location #1 FF Outlet Method Mod. 101A
 Individual Tare of Reagent 200 (ml)(gm) of KCl
 Individual Tare of Reagent 100 (ml)(gm) of KCl
 Individual Tare of Reagent 200 (ml)(gm) of 47% KMnO4 / 109% H2SO4
 Individual Tare of Silca Gel 200 gm

Other (specify)

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
<u>1-D-mm10141</u>	<u>3/19/98</u>	<u>NA</u>	<u>NA</u>	<u>Y</u>	<u>HD</u>	<u>3/19/98</u>	<u>10</u>	<u>Y</u>	<u>HD</u>
				Filter Appearance* <u>clean</u>					
				Reagent Appearance* <u>ok</u>					
<u>2-D-mm10142</u>	<u>3/19/98</u>	<u>NA</u>	<u>NA</u>	<u>Y</u>	<u>HD</u>	<u>3/19</u>	<u>20</u>	<u>Y</u>	<u>HD</u>
				Filter Appearance* <u>same</u>					
				Reagent Appearance* <u>ok</u>					
<u>2-D-mm10143</u>									
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					

ABORTED

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed)

REMARKS

RECORD OF CUSTODY, CONTAINER No. 206

Client OGDEN MARTIN SYSTEMS

Job No. 10388

Plant Name OMS - LAKE

City/State OKAHUMPKA, FL

Sampling Method (s) # 2 FF outlet (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002131	3/14/98	0742	S	<i>[Signature]</i>	
	3/18/98	1600	B	<i>[Signature]</i>	change train's
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **
_____	_____	_____	Yes ___ No ___ N/A ___
Signature	Date	Time	

As Applicable:
 All liquid levels at mark (✓) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
 TUBE SAMPLES put in freezer by _____ Date _____ Time _____
 CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name

OMS-LAKE

Job No.

10388

City/State

OKAHUMPKA, FL

Sampling Loc.

#1 SDA Inkt + FFC

Run Number

1-I-MMD14-7

1-O-MMD14-7

Sampling Date

3/20/98

3/20/98

Analysis Date

3/20/98

3/20/98

Analyst

HTD

HTD

<u>Reagent 1 (KCl Imp 1+2)</u>	Final Weight, g	391.7	422.8
	Tared Weight, g	255.5	257.3
	Water Catch, g	136.2	165.5
<u>Reagent 2 (KCl Imp 3)</u>	Final Weight, g	149.7	146.4
	Tared Weight, g	140.3	140.4
	Water Catch, g	9.4	6.0
<u>Reagent 3 (KMnO4)</u>	Final Weight, g	609.9	600.0
	Tared Weight, g	606.2	599.7
	Water Catch, g	3.7	0.3
CONDENSED WATER, g		149.3	171.8
<u>Silica Gel</u>	Final Weight, g	209.7	210.0
	Tared Weight, g	200.0	200.0
	Water Catch, g	9.7	10.0
TOTAL WATER COLLECTED, g		159.0	181.8

Balance No.

3

Type (✓) Triple Beam

Electronic

Reagent Box

211

Balance located in stable, draft-free area (✓)?

Yes

No

(If "No," explain below)

Comments

balance in lab trailer

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10388

City / State OKAHUMPKA, FL Sampling Loc. #1 FF outlet

Run Number	<u>1-0-mm101A-4</u>	<u>1-0-mm101A-5</u>	<u>1-0-mm101A-6</u>
Sampling Date	<u>3/20/98</u>	<u>3/20/98</u>	<u>3/20/98</u>
Analysis Date	<u>3/20/98</u>	<u>3/20/98</u>	<u>3/20/98</u>
Analyst	<u>SLB</u>	<u>HTD</u>	<u>HTD</u>

<u>Reagent 1 (KCl 1st + 2nd Imp)</u>			
Final Weight, g	<u>426.6</u>	<u>410.0</u>	<u>422.4</u>
Tared Weight, g	<u>257.5</u>	<u>257.4</u>	<u>259.3</u>
Water Catch, g	<u>169.1</u>	<u>152.6</u>	<u>163.1</u>
<u>Reagent 2 (KCl 3rd Imp)</u>			
Final Weight, g	<u>144.1</u>	<u>155.4</u>	<u>148.6</u>
Tared Weight, g	<u>142.5</u>	<u>136.0</u>	<u>141.8</u>
Water Catch, g	<u>1.6</u>	<u>19.4</u>	<u>6.8</u>
<u>Reagent 3 (KMnO₄ / H₂SO₄)</u>			
Final Weight, g	<u>610.0</u>	<u>610.4</u>	<u>605.7</u>
Tared Weight, g	<u>601.7</u>	<u>600.2</u>	<u>600.0</u>
Water Catch, g	<u>8.3</u>	<u>10.2</u>	<u>5.7</u>
CONDENSED WATER, g	<u>179.0</u>	<u>182.0</u>	<u>1785.6</u>
<u>Silica Gel</u>			
Final Weight, g	<u>209.7</u>	<u>209.7</u>	<u>209.9</u>
Tared Weight, g	<u>200.0</u>	<u>200.0</u>	<u>200.0</u>
Water Catch, g	<u>9.7</u>	<u>9.7</u>	<u>9.9</u>
TOTAL WATER COLLECTED, g	<u>188.7</u>	<u>191.9</u>	<u>185.5</u>

Balance No. CEM 3 Type (✓) Triple Beam Electronic Reagent Box 207

Balance located in stable, draft-free area (✓)? Yes No (If "No," explain below.)

Comments _____

FIELD SAMPLE RECOVERY QUALITY CONTROL

Box No. 207 Assembly Date 3/14/98 Assembled By G. MATA
 Client OGDEN MARTIN SYSTEMS Job No. 10388
 Plant OMS - LAKE City / State OKAHOMPKA, FL
 Sampling Location #1 FF Outlet Method 101A

Individual Tare of Reagent 200 (ml) (gm) of KCl
 Individual Tare of Reagent 100 (ml) (gm) of KCl
 Individual Tare of Reagent 200 (ml) (gm) of ~~KMnO4~~ / H2SO4
 Individual Tare of Silca Gel 200 gm

Other (specify)

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
1-0-mm1014-4	3/20	NA	NA	✓	SCG	3/20	20	✓	SCG
1-0-mm1014-5	3/20			✓	HD	3/20	25	✓	HD
1-0-mm1014-6	3/20			✓	HD	3/20	30	✓	HD
1-0-mm ¹⁰¹⁴ 14-7	3/20			✓	HD	3/20	25	✓	HD

Filter Appearance*

NA

Reagent Appearance*

Clear

Filter Appearance*

same

Reagent Appearance*

same

Filter Appearance*

same

Reagent Appearance*

same

Filter Appearance*

same

Reagent Appearance*

same

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS

Client OGDEN MARTIN SYSTEMS

Job No. 10388

Plant Name OMS - LAKE

City/State OKLAHOMA, FL

Sampling Method (s) Mod. 101A

(EPA, NIOSH, etc.)

Container Type (v) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002040	3/14/98	3:15	S	<i>[Signature]</i>	change train
	3/18/98	0900	B	<i>[Signature]</i>	
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **		
_____	_____	_____	Yes	No	N/A
Signature	Date	Time			

As Applicable:
All liquid levels at mark (v) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____

CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10388
 City / State OKAHUMPKA, FL Sampling Loc. #2 SDA Inlet

Run Number	<u>2-I-m101A-1</u>	<u>2-I-m101A-2</u>	<u>2-I-m101A-3</u>
Sampling Date	<u>3/18/98</u>		
Analysis Date	<u>"</u>		
Analyst	<u>SLG/HTM</u>		

<u>Reagent 1 (4% KMnO4/10% H2SO4)</u>	Final Weight, g <u>704.1</u>		
	Tared Weight, g <u>603.4</u>	<u>605.3</u>	<u>600.4</u>
	Water Catch, g <u>100.7</u>		
<u>Reagent 2 (_____)</u>	Final Weight, g _____		
	Tared Weight, g _____		
	Water Catch, g _____		
<u>Reagent 3 (_____)</u>	Final Weight, g _____		
	Tared Weight, g _____		
	Water Catch, g _____		
<u>CONDENSED WATER, g</u>	<u>100.7</u>		
<u>Silica Gel</u>	Final Weight, g <u>215.1</u>		
	Tared Weight, g <u>200.0</u>	<u>200.0</u>	<u>200.0</u>
	Water Catch, g <u>15.1</u>		
<u>TOTAL WATER COLLECTED, g</u>	<u>115.8</u> ✓		

Balance No. 3 Type (✓) Triple Beam Electronic _____ Reagent Box 214
 Balance located in stable, draft-free area (✓)? Yes No _____ (If "No," explain below)

Comments Balance in lab trailer D-15

Box No. 214 Assembly Date 3/14/98 Assembled By G. MATA
 Client OGDEN MARTIN SYSTEMS Job No. 10388
 Plant OMS - LAKE City / State OKAHUMPKA, FL
 Sampling Location #2 SDA Inlet Method 101A
 Individual Tare of Reagent 200 (ml) (gm) of 47% KMnO4 / 109% H2SO4
 Individual Tare of Reagent 100 (ml) (gm) of KCl
 Individual Tare of Reagent 200 (ml) (gm) of KCl
 Individual Tare of Silca Gel 200 gm

Other (specify)

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
<u>2-I-M101A-1</u>	<u>3/18/98</u>	<u>NA</u>	<u>NA</u>	<u>Y</u>	<u>HD</u>	<u>3/18</u>	<u>30</u>	<u>Y</u>	<u>HD</u>
				Filter Appearance*					
				<u>duty inlet filter</u>					
				Reagent Appearance*					
				<u>ok</u>					
<u>2-I-M101A-2</u>		<u>NA</u>	<u>NA</u>	<u>Y</u>	<u>HD</u>	<u>3/18</u>	<u>25</u>	<u>Y</u>	<u>HD</u>
				Filter Appearance*					
				<u>same</u>					
				Reagent Appearance*					
				<u>same</u>					
<u>2-I-M101A-3</u>									
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS

RECORD OF CUSTODY, CONTAINER No. 214

Client OGDEN MARTIN SYSTEMS

Job No. 10388

Plant Name OMS - LAKE

City/State OKAHUMPKA, FL

Sampling Method (s) 101A

EPA, NIOSH, etc.)

Container Type (v) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002421	3/14/98	0756	S	<i>[Signature]</i>	
	3/18/98	1000	B	<i>[Signature]</i>	change train
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody

* S = Sealed By; B = Broken

** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **
_____	_____	_____	Yes ___ No ___ N/A ___
Signature	Date	Time	

As Applicable:

All liquid levels at mark (v) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:

TUBE SAMPLES put in freezer by _____ Date _____ Time _____

CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

MOISTURE ANALYTICAL RESULTS

Plant Name OMS-LAKE Job No. 10388
 City/State OKAHUMPKA, FL Sampling Loc. #2 FF outlet

Run Number	<u>2-D-m1014-1</u>	2-D-m1014-2	<u>2-D-m1014-3</u>
Sampling Date	<u>3/18/98</u>		
Analysis Date	<u>3/18/98</u>		
Analyst	<u>HTD</u>		

<u>Reagent 1 (4% KMnO₄/10% H₂SO₄)</u>			
Final Weight, g	<u>710.0</u>		
Tared Weight, g	<u>604.7</u>	<u>600.3</u>	<u>603.6</u>
Water Catch, g	<u>105.3</u>		
<u>Reagent 2 ()</u>			
Final Weight, g			
Tared Weight, g			
Water Catch, g			
<u>Reagent 3 ()</u>			
Final Weight, g			
Tared Weight, g			
Water Catch, g			
CONDENSED WATER, g	<u>105.3</u>		
<u>Silica Gel</u>			
Final Weight, g	<u>210.3</u>		
Tared Weight, g	<u>200.0</u>	<u>200.0</u>	<u>200.0</u>
Water Catch, g	<u>10.3</u>		
TOTAL WATER COLLECTED, g	<u>115.6</u> ✓		

Balance No. 3 Type (✓) Triple Beam Electronic Reagent Box M147
 Balance located in stable, draft-free area (✓)? Yes No (If "No," explain below.)

Comments balance in lab trailer

FIELD SAMPLE RECOVERY QUALITY CONTROL

Box No. M147 Assembly Date 3/14/98 Assembled By G. MATA
 Client OGDEN MARTIN SYSTEMS Job No. 10388
 Plant OMS - LAKE City / State OKAHUMPKA, FL
 Sampling Location #2 FF Outlet Method 101A
 Individual Tare of Reagent 200 (ml) (gm) of 49% $K_2Cr_2O_7$ / 10% H_2SO_4
 Individual Tare of Reagent 100 (ml) (gm) of KCl
 Individual Tare of Reagent 200 (ml) (gm) of KCl
 Individual Tare of Silca Gel 200 gm

Other (specify)

Run Number	Run Date	Filter or XAD		Liquid Tare at Mark?	Inits.	Sample Recovery Date	% Sil. Gel Spent	Liquid Level Marked	Initials
		Number	Tare, grams						
<u>2-0-M101A-1</u>	<u>3/18/98</u>	<u>NA</u>	<u>NA</u>	<u>Y</u>	<u>HD</u>	<u>3/18</u>	<u>20</u>	<u>Y</u>	<u>HD</u>
				Filter Appearance*					
				<u>clean</u>					
				Reagent Appearance*					
				<u>ok</u>					
<u>HD</u> <u>2-0-M101A-2</u>	<u>3/18/98</u>	<u>NA</u>	<u>NA</u>	<u>Y</u>	<u>HD</u>	<u>3/18</u>	<u>25</u>	<u>Y</u>	<u>HD</u>
				Filter Appearance*					
				<u>SAME</u>					
				Reagent Appearance*					
				<u>SAME</u>					
<u>HD</u> <u>2-0-M101A-3</u>									
				Filter Appearance*					
				Reagent Appearance*					
				Filter Appearance*					
				Reagent Appearance*					

* Use "REMARKS" section if needed.

All liquid levels at mark? (circle) YES NO (estimate loss if not at mark; use "REMARKS" section if needed.)

REMARKS

RECORD OF CUSTODY, CONTAINER No. M147

Client OGDEN MARTIN SYSTEMS

Job No. 10388

Plant Name OMS - LAKE

City/State OKLAHOMA, FL

Sampling Method (s) 1014

(EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002093	3/14/98	0753	S	<i>[Signature]</i>	
	3/18/98	1000	B	<i>[Signature]</i>	change train
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **
_____	_____	_____	Yes ___ No ___ N/A ___
Signature	Date	Time	

As Applicable:
All liquid levels at mark (✓) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____

CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

RECORD OF CUSTODY, CONTAINER No. 632

Client OGDEN MARTIN SYSTEMS

Job No. 10388

Plant Name OMS - LAKE

City/State OKLAHOMA, FL

Sampling Method (s) #2 SDA Inlet (EPA, NIOSH, etc.)

Container Type (v) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002096	3/14/98	0821	S	<i>[Signature]</i>	
	3/18/98	1600	B	<i>[Signature]</i>	
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact?**
_____	_____	_____	Yes ___ No ___ N/A ___
Signature	Date	Time	

As Applicable:
All liquid levels at mark (v) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____
CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

Client OGDEN MARTIN SYSTEMS

Job No. 10388

Plant Name OMS - LAKE

City/State OKLAHOMA, FL

Sampling Method (s) # 2 FF Outlet (EPA, NIOSH, etc.)

Container Type (✓) Reagent Box Cooler Other (specify) _____

Seal No. or "PC"	Date	Time	*	Full Signature	Reason for Breaking Seal**
0002879	3/14/98	0850	S	<i>[Signature]</i>	
	3/18/98	1600	B	<i>[Signature]</i>	<i>change train</i>
			S		
			B		
			S		
			B		
			S		
			B		
			S		
			B		

PC = Personal Custody * S = Sealed By; B = Broken ** Use "REMARKS" Section if more space needed

Container Received by AirKinetics Sample Custodian			Seal Intact? **
_____	_____	_____	Yes ___ No ___ N/A ___
Signature	Date	Time	

As Applicable:
All liquid levels at mark (✓) Yes ___ No ___ (Estimate loss if not at mark; describe in "REMARKS")

As Applicable:
TUBE SAMPLES put in freezer by _____ Date _____ Time _____
CONDENSATE SAMPLES put in refridge. by _____ Date _____ Time _____

REMARKS _____

APPENDIX D

ANALYTICAL DATA

2.0 QUANTERRA ENVIRONMENTAL SERVICES

Quanterra Incorporated
880 Riverside Parkway
West Sacramento, California 95605

916 373-5600 Telephone
916 372-1059 Fax

March 31, 1998

QUANTERRA INCORPORATED PROJECT NUMBER: 098134

PO NUMBER: 679-SG Job #10388

Gary Mata
AirKinetics, Inc.
5932 Bolsa Avenue
Suite 105
Huntington Beach, CA 92649

Dear Mr. Mata:

This report contains the analytical results for the eight airtrain samples which were received under chain of custody by Quanterra Incorporated on 20 March 1998.

The case narrative is an integral part of this report.

If you have any questions, please feel free to call.

Sincerely,



Robert Weidenfeld
Project Manager
Advanced Technology

RW/rr

TABLE OF CONTENTS

QUANTERRA INCORPORATED PROJECT NUMBER 098134

Case Narrative

Quanterra's Quality Assurance Program

Sample Description Information

Chain of Custody Documentation

Summary Report

Metals Emission from Stationary Sources

Includes Sample: 1 through 8

Sample Data

QC Lot Assignment Report

CASE NARRATIVE

QUANTERRA INCORPORATED PROJECT NUMBER 098134

The matrix spike result was not calculated for the front half fraction due to the high level of mercury in the sample compared to the spike.

There were no additional anomalies associated with this report.

QUANTERRA INCORPORATED QUALITY CONTROL PROGRAM

Quanterra has implemented an extensive Quality Control (QC) program to ensure the production of scientifically sound, legally defensible data of known documentable quality. This QC program is based upon requirements in "Test Methods for Evaluating Solid Waste", USEPA SW-846, Third Edition. It applies whenever SW-846 analytical methods are used. It also applies in whole or in part whenever project requirements fail to specify some aspect of QC practices described here. It does not apply when other well defined QC programs (e.g. CLP or CLP-like) are specified. This is Quanterra's base QC program for environmental analysis.

Definitions:

Quality Control Batch. The quality control (QC) batch is a set of up to 20 field samples plus associated laboratory QC samples that are similar in composition (matrix) and that are processed within the same time period with the same reagent and standard lots.

Surrogate. A surrogate (or internal standard) is an organic compound similar in chemical behavior to the target analyte, but not normally found in environmental samples. Surrogates (or IS) are added to all samples in a batch to monitor the effects of both the matrix and the analytical process on accuracy.

Method Blank. A method blank (MB) is a control sample prepared using the same reagents used for the samples. As part of the QC batch, it accompanies the samples through all steps of the sample extraction and cleanup procedure. The method blank is used to monitor the level of contamination introduced to a batch of samples as a result of processing in the laboratory.

Laboratory Control Sample. A laboratory control sample (LCS) is prepared using a well characterized matrix (e.g., reagent water or Ottawa sand) that is spiked with known amounts of representative analytes. Alternate matrices (e.g., glass beads) may be used for soil analyses when Ottawa sand is not appropriate. As part of a QC batch, it accompanies the samples through all steps of the sample extraction and cleanup process. The LCS is used to monitor the accuracy of the analytical process independent of possible interference effects due to sample matrix.

Duplicate Control Sample. A duplicate laboratory control sample (DCS) consists of a pair of LCSs analyzed within the same QC batch to monitor precision and accuracy independent of sample matrix effects.

SAMPLE DESCRIPTION INFORMATION
for
AirKinetics, Inc.

Lab ID	Client ID	Matrix	Sampled Date	Time	Received Date
098134-0001-SA	2-O-M101A-1	AIRTRAIN	18 MAR 98		19 MAR 98
098134-0002-SA	2-I-M101A-1	AIRTRAIN	18 MAR 98		19 MAR 98
098134-0003-SA	1-I-MM101A-1	AIRTRAIN	19 MAR 98		19 MAR 98
098134-0003-MS	1-I-MM101A-1	AIRTRAIN	19 MAR 98		19 MAR 98
098134-0004-SA	1-I-MM101A-2	AIRTRAIN	19 MAR 98		19 MAR 98
098134-0005-SA	1-O-MM101A-1	AIRTRAIN	19 MAR 98		19 MAR 98
098134-0006-SA	1-O-MM101A-2	AIRTRAIN	19 MAR 98		19 MAR 98
098134-0007-SA	2-I-MM101A-1	AIRTRAIN	18 MAR 98		19 MAR 98
098134-0008-SA	2-O-MM101A-1	AIRTRAIN	18 MAR 98		19 MAR 98

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-I-MM101A-1
Lab ID: 098134-0003-MS
Matrix: AIRTRAIN
Authorized: 20 MAR 98

Sampled: 19 MAR 98
Prepared: See Below

Received: 19 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
<i>Oxidiz.</i> Mercury, KCl (3)	0.61	ug/Sample	0.034	7471	21 MAR 98	22 MAR 98
<i>Oxidiz.</i> Mercury, KCl (1&2)	84.6	ug/Sample	49.0	7471	22 MAR 98	22 MAR 98 o
<i>Element</i> → Mercury, KMNO4	5.4	ug/Sample	1.0	7471	22 MAR 98	22 MAR 98
<i>Element</i> → Mercury, FH	27.0	ug/sample	6.0	7471	22 MAR 98	22 MAR 98 o
<i>Elemental</i> Mercury, HCL	2.0	ug/Sample	0.50	7471	23 MAR 98	23 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-I-MM101A-1
Lab ID: 098134-0003-SA
Matrix: AIRTRAIN
Authorized: 20 MAR 98

Sampled: 19 MAR 98
Prepared: See Below

Received: 19 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (1&2)	36.0	ug/Sample	9.8	7471	22 MAR 98	22 MAR 98 o
Mercury, KCl (3)	0.44	ug/Sample	0.034	7471	21 MAR 98	22 MAR 98
Mercury, KMNO4	4.4	ug/Sample	0.20	7471	22 MAR 98	22 MAR 98
Mercury, FH	27.3	ug/sample	1.2	7471	22 MAR 98	22 MAR 98 o
Mercury, HCL	1.6	ug/Sample	0.10	7471	23 MAR 98	23 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-I-MM101A-2
Lab ID: 098134-0004-SA
Matrix: AIRTRAIN
Authorized: 20 MAR 98

Sampled: 19 MAR 98
Prepared: See Below

Received: 19 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (1&2)	531	ug/Sample	18.1	7471	22 MAR 98	22 MAR 98 o
Mercury, KCl (3)	3.9	ug/Sample	0.17	7471	21 MAR 98	22 MAR 98 o
Mercury, KMNO4	8.7	ug/Sample	0.20	7471	22 MAR 98	22 MAR 98
Mercury, FH	104	ug/sample	12.0	7471	22 MAR 98	22 MAR 98 o
Mercury, HCL	0.26	ug/Sample	0.10	7471	23 MAR 98	23 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-O-MM101A-1
Lab ID: 098134-0005-SA
Matrix: AIRTRAIN
Authorized: 20 MAR 98

Sampled: 19 MAR 98
Prepared: See Below

Received: 19 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (3)	0.55	ug/Sample	0.034	7471	21 MAR 98	22 MAR 98
Mercury, KCl (1&2)	29.1	ug/Sample	0.83	7471	22 MAR 98	22 MAR 98
Mercury, KMNO4	ND	ug/Sample	0.20	7471	22 MAR 98	22 MAR 98
Mercury, HCL	ND	ug/Sample	0.10	7471	23 MAR 98	23 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
 Client ID: 1-O-MM101A-2
 Lab ID: 098134-0006-SA
 Matrix: AIRTRAIN
 Authorized: 20 MAR 98

Sampled: 19 MAR 98
 Prepared: See Below

Received: 19 MAR 98
 Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (3)	0.35	ug/Sample	0.032	7471	21 MAR 98	22 MAR 98
Mercury, KCl (1&2)	36.2	ug/Sample	1.2	7471	22 MAR 98	22 MAR 98 o
Mercury, KMNO4	ND	ug/Sample	0.20	7471	22 MAR 98	22 MAR 98
Mercury, HCL	ND	ug/Sample	0.10	7471	23 MAR 98	23 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
 NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
 Rev 230787

QC LOT ASSIGNMENT REPORT
Metals Analysis and Preparation

Laboratory Sample Number	QC Matrix	QC Category	QC Lot Number (DCS)	QC Run Number (SCS/BLANK)
098134-0001-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0001-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098134-0002-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0002-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098134-0003-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0003-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0003-SA	AQUEOUS	HG-TRC-G	21 MAR 98-U	21 MAR 98-U
098134-0003-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0003-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098134-0003-MS	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0003-MS	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0003-MS	AQUEOUS	HG-TRC-G	21 MAR 98-U	21 MAR 98-U
098134-0003-MS	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0003-MS	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098134-0004-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0004-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0004-SA	AQUEOUS	HG-TRC-G	21 MAR 98-U	21 MAR 98-U
098134-0004-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0004-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098134-0005-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0005-SA	AQUEOUS	HG-TRC-G	21 MAR 98-U	21 MAR 98-U
098134-0005-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0005-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098134-0006-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0006-SA	AQUEOUS	HG-TRC-G	21 MAR 98-U	21 MAR 98-U
098134-0006-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0006-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098134-0007-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0007-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0007-SA	AQUEOUS	HG-TRC-G	21 MAR 98-U	21 MAR 98-U
098134-0007-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0007-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098134-0008-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0008-SA	AQUEOUS	HG-TRC-G	21 MAR 98-U	21 MAR 98-U
098134-0008-SA	AQUEOUS	HG-TRC-G	21 MAR 98-T	21 MAR 98-T
098134-0008-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T

METHOD BLANK REPORT
Metals Analysis and Preparation

Analyte	Result	Units	Reporting Limit
Test: HG-CVAA-KMNO4-AIRTRA Matrix: AIRTRAIN QC Lot: 21 MAR 98-T QC Run: 21 MAR 98-T			
Mercury, KMNO4	ND	ug/Sample	0.20
Test: HG-CVAA-HCL-AIRTRAIN Matrix: AIRTRAIN QC Lot: 23 MAR 98-T QC Run: 23 MAR 98-T			
Mercury, HCL	ND	ug/Sample	0.20
Test: HG-CVAA-FH-AIRTRAIN Matrix: AIRTRAIN QC Lot: 21 MAR 98-T QC Run: 21 MAR 98-T			
Mercury, FH	ND	ug/sample	0.20
Test: HG-CVAA-KCL(1&2)-AIR Matrix: AIRTRAIN QC Lot: 21 MAR 98-T QC Run: 21 MAR 98-T			
Mercury, KCl (1&2)	ND	ug/Sample	0.20
Test: HG-CVAA-KCL(3)-AIR Matrix: AIRTRAIN QC Lot: 21 MAR 98-U QC Run: 21 MAR 98-U			
Mercury, KCl (3)	ND	ug/Sample	0.20
Test: HG-CVAA-KMNO4-AIRTRA Matrix: AIRTRAIN QC Lot: 21 MAR 98-T QC Run: 21 MAR 98-T			
Mercury, KMNO4	ND	ug/Sample	0.20

METHOD BLANK REPORT
Metals Analysis and Preparation (cont.)

Analyte	Result	Units	Reporting Limit
Test: HG-CVAA-HCL-AIRTRAIN Matrix: AIRTRAIN QC Lot: 23 MAR 98-T QC Run: 23 MAR 98-T			
Mercury, HCL	ND	ug/Sample	0.20
Test: HG-CVAA-FH-AIRTRAIN Matrix: AIRTRAIN QC Lot: 21 MAR 98-T QC Run: 21 MAR 98-T			
Mercury, FH	ND	ug/sample	0.20
Test: HG-CVAA-KCL(1&2)-AIR Matrix: AIRTRAIN QC Lot: 21 MAR 98-T QC Run: 21 MAR 98-T			
Mercury, KCl (1&2)	ND	ug/Sample	0.20
Test: HG-CVAA-KCL(3)-AIR Matrix: AIRTRAIN QC Lot: 21 MAR 98-U QC Run: 21 MAR 98-U			
Mercury, KCl (3)	ND	ug/Sample	0.20
Test: HG-CVAA-KMNO4-AIRTRA Matrix: AIRTRAIN QC Lot: 21 MAR 98-T QC Run: 21 MAR 98-T			
Mercury, KMNO4	ND	ug/Sample	0.20
Test: HG-CVAA-HCL-AIRTRAIN Matrix: AIRTRAIN QC Lot: 23 MAR 98-T QC Run: 23 MAR 98-T			
Mercury, HCL	ND	ug/Sample	0.20

METHOD BLANK REPORT
Metals Analysis and Preparation (cont.)

Analyte	Result	Units	Reporting Limit
Test: HG-CVAA-KCL(1&2)-AIR Matrix: AIRTRAIN QC Lot: 21 MAR 98-T QC Run: 21 MAR 98-T			
Mercury, KCl (1&2)	ND	ug/Sample	0.20
Test: HG-CVAA-KCL(3)-AIR Matrix: AIRTRAIN QC Lot: 21 MAR 98-U QC Run: 21 MAR 98-U			
Mercury, KCl (3)	ND	ug/Sample	0.20
Test: HG-CVAA-KMNO4-AIRTRA Matrix: AIRTRAIN QC Lot: 21 MAR 98-T QC Run: 21 MAR 98-T			
Mercury, KMNO4	ND	ug/Sample	0.20
Test: HG-CVAA-HCL-AIRTRAIN Matrix: AIRTRAIN QC Lot: 23 MAR 98-T QC Run: 23 MAR 98-T			
Mercury, HCL	ND	ug/Sample	0.20

DUPLICATE CONTROL SAMPLE REPORT
Metals Analysis and Preparation

Analyte	Concentration Spiked	Concentration Measured		AVG	Accuracy Average(%)		Precision (RPD)	
		DCS1	DCS2		DCS	Limits	DCS	Limit
Category: HG-TRC-G								
Matrix: AQUEOUS								
QC Lot: 21 MAR 98-T								
Concentration Units: ug/L								
Mercury	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, BH	1.0	0.995	0.998	0.996	100	80-120	0.3	20.0
Mercury, Condensate	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, FH	1.0	0.995	0.998	0.996	100	80-120	0.3	20.0
Mercury, FHBH	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, HCL	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, KMNO4	1.0	0.995	0.998	0.996	100	80-120	0.3	20.0

Category: HG-TRC-G
Matrix: AQUEOUS
QC Lot: 23 MAR 98-T
Concentration Units: ug/L

Mercury	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, BH	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, Condensate	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, FH	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, FHBH	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, HCL	1.0	0.969	0.972	0.970	97	80-120	0.3	20.0
Mercury, KMNO4	1.0	0.969	0.972	0.970	97	80-120	0.3	20.0

Category: HG-TRC-G
Matrix: AQUEOUS
QC Lot: 21 MAR 98-U
Concentration Units: ug/L

Mercury	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, BH	1.0	0.963	0.974	0.968	97	80-120	1.1	20.0
Mercury, Condensate	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, FH	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, FHBH	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, HCL	1.0	NA	NA	NC	NC	80-120	NC	20.0
Mercury, KMNO4	1.0	NA	NA	NC	NC	80-120	NC	20.0

The analyte was positively identified, the quantitation is an estimation.

NC = Not calculated, calculation not applicable.

The data are unusable due to deficiencies in the ability to analyze the sample and meet QC criteria.

Calculations are performed before rounding to avoid round-off errors in calculated results.

MATRIX SPECIFIC QC
ASSIGNMENT REPORT
Metals Analysis and Preparation

QC SAMPLE TYPE	TEST	LABORATORY SAMPLE NUMBER	QC LOT
MATRIX SPIKE	HG-CVAA-FH-AIRTRAIN	098134-0003-MS	21 MAR 98-T
MATRIX SPIKE	HG-CVAA-KCL(1&2)-AIR	098134-0003-MS	21 MAR 98-T
MATRIX SPIKE	HG-CVAA-KCL(3)-AIR	098134-0003-MS	21 MAR 98-U
MATRIX SPIKE	HG-CVAA-KMNO4-AIRTRA	098134-0003-MS	21 MAR 98-T
MATRIX SPIKE	HG-CVAA-HCL-AIRTRAIN	098134-0003-MS	23 MAR 98-T

MATRIX SPIKE REPORT
Metals Analysis and Preparation

Analyte	Sample	Concentration Matrix Spike	Amount Spiked	% Rec
Test: HG-CVAA-FH-AIRTRAIN Matrix AIRTRAIN Sample: 098134-0003 Units: ug/sample				
Mercury, FH	27.3	27.0	6.0	NC
Test: HG-CVAA-KCL(1&2)-AIR Matrix AIRTRAIN Sample: 098134-0003 Units: ug/Sample				
Mercury, KCl (1&2)	36.0	84.6	49.0	99
Test: HG-CVAA-KCL(3)-AIR Matrix AIRTRAIN Sample: 098134-0003 Units: ug/Sample				
Mercury, KCl (3)	0.44	0.61	0.17	100
Test: HG-CVAA-KMNO4-AIRTRA Matrix AIRTRAIN Sample: 098134-0003 Units: ug/Sample				
Mercury, KMNO4	4.4	5.4	1.0	100
Test: HG-CVAA-HCL-AIRTRAIN Matrix AIRTRAIN Sample: 098134-0003 Units: ug/Sample				
Mercury, HCL	1.6	2.0	0.50	80

All calculations are performed before rounding to avoid round-off errors in calculated results.

AirKinetics, Inc.

EMISSIONS CHARACTERIZATION AND TESTING SERVICES

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 679-SG JOB NAME: Ogden - Lake

LABORATORY: Quanterra Environ. Services JOB No.: 10388

DATE SAMPLES WERE TRANSMITTED: 19-Mar-98 EXPECTED DATE OF RESULTS: 24-Mar-98

SAMPLE MATRIX: 0.1 N KCl, 4% KMnO4 / 10% H2SO4, 0.1N HNO3, 8N HCl

TYPE OF ANALYSIS REQUIRED: Please analyze according to EPA Method 101A for Hg only.

Sample / Run ID #	Sample Collection Date	Sample Components	Sample Matrix	Condition of Samples *
1-I-MM101A-1	3/19/98	Front Half Rinse	0.1N HNO3	Preserved with KMnO4
		Filter	Filter	
		1st and 2nd Imp.	0.1N KCl	
		3rd Impinger	0.1 N KCl	
		KMnO4	KMnO4 / H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	
1-O-MM101A-1	3/19/98	1st and 2nd Imp.	0.1 N KCl	Preserved with KMnO4
		3rd Impinger	0.1 N KCl	Preserved with KMnO4
		KMnO4	KMnO4 / H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	
1-I-MM101A-2	3/19/98	Front Half Rinse	0.1N HNO3	Preserved with KMnO4
		Filter	Filter	
		1st and 2nd Imp.	0.1N KCl	
		3rd Impinger	0.1 N KCl	
		KMnO4	KMnO4 / H2SO4	
		8N HCl Rinse	8 N HCl w/ DI	

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: [Signature] Date/Time: 3/19/98

Transported by: FedEx Date/Time: _____

Transported to: Quanterra Environmental Services
880 Riverside Parkway
West Sacramento, CA 95605-1501

Received by: [Signature] Date/Time: 032098 1130

Quanterra Incorporated
880 Riverside Parkway
West Sacramento, California 95605

916 373-5600 Telephone
916 372-1059 Fax

March 30, 1998

QUANTERRA INCORPORATED PROJECT NUMBER: 098186
PO NUMBER: 679-SG Job # 10388

Gary Mata
AirKinetics, Inc.
5932 Bolsa Avenue
Suite 105
Huntington Beach, CA 92649

Dear Mr. Mata:

This report contains the analytical results for the ten airtrain samples which were received under chain of custody by Quanterra Incorporated on 21 March 1998.

The case narrative is an integral part of this report.

If you have any questions, please feel free to call.

Sincerely,



Robert Weidenfeld
Project Manager
Advanced Technology

RW/rr

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QUANTERRA INCORPORATED PROJECT NUMBER 098186

Case Narrative

Quanterra's Quality Assurance Program

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Chain of Custody Documentation

Summary Report

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Includes Sample: 1 through 10

Sample Data

QC Lot Assignment Report

CASE NARRATIVE

QUANTERRA INCORPORATED PROJECT NUMBER 098186

With the exception of the HCl fraction, the % recoveries for the matrix spikes were not calculated due to the high level of analyte in the sample compared to the spike.

There were no additional anomalies associated with this report.

QUANTERRA INCORPORATED QUALITY CONTROL PROGRAM

Quanterra has implemented an extensive Quality Control (QC) program to ensure the production of scientifically sound, legally defensible data of known documentable quality. This QC program is based upon requirements in "Test Methods for Evaluating Solid Waste", USEPA SW-846, Third Edition. It applies whenever SW-846 analytical methods are used. It also applies in whole or in part whenever project requirements fail to specify some aspect of QC practices described here. It does not apply when other well defined QC programs (e.g. CLP or CLP-like) are specified. This is Quanterra's base QC program for environmental analysis.

Definitions:

Quality Control Batch. The quality control (QC) batch is a set of up to 20 field samples plus associated laboratory QC samples that are similar in composition (matrix) and that are processed within the same time period with the same reagent and standard lots.

Surrogate. A surrogate (or internal standard) is an organic compound similar in chemical behavior to the target analyte, but not normally found in environmental samples. Surrogates (or IS) are added to all samples in a batch to monitor the effects of both the matrix and the analytical process on accuracy.

Method Blank. A method blank (MB) is a control sample prepared using the same reagents used for the samples. As part of the QC batch, it accompanies the samples through all steps of the sample extraction and cleanup procedure. The method blank is used to monitor the level of contamination introduced to a batch of samples as a result of processing in the laboratory.

Laboratory Control Sample. A laboratory control sample (LCS) is prepared using a well characterized matrix (e.g., reagent water or Ottawa sand) that is spiked with known amounts of representative analytes. Alternate matrices (e.g., glass beads) may be used for soil analyses when Ottawa sand is not appropriate. As part of a QC batch, it accompanies the samples through all steps of the sample extraction and cleanup process. The LCS is used to monitor the accuracy of the analytical process independent of possible interference effects due to sample matrix.

Duplicate Control Sample. A duplicate laboratory control sample (DCS) consists of a pair of LCSs analyzed within the same QC batch to monitor precision and accuracy independent of sample matrix effects.

SAMPLE DESCRIPTION INFORMATION
for
AirKinetics, Inc.

Lab ID	Client ID	Matrix	Sampled		Received
			Date	Time	
098186-0001-SA	1-O-MM101A-FB	AIRTRAIN	20 MAR 98		21 MAR 98
098186-0002-SA	Reagent Blanks	AIRTRAIN	20 MAR 98		21 MAR 98
098186-0003-SA	1-O-MM101A-4	AIRTRAIN	20 MAR 98		21 MAR 98
098186-0004-SA	1-O-MM101A-5	AIRTRAIN	20 MAR 98		21 MAR 98
098186-0005-SA	1-O-MM101A-6	AIRTRAIN	20 MAR 98		21 MAR 98
098186-0006-SA	1-O-MM101A-7	AIRTRAIN	20 MAR 98		21 MAR 98
098186-0007-SA	1-I-MM101A-4	AIRTRAIN	20 MAR 98		21 MAR 98
098186-0007-MS	1-I-MM101A-4	AIRTRAIN	20 MAR 98		21 MAR 98
098186-0008-SA	1-I-MM101A-5	AIRTRAIN	20 MAR 98		21 MAR 98
098186-0009-SA	1-I-MM101A-6	AIRTRAIN	20 MAR 98		21 MAR 98
098186-0010-SA	1-I-MM101A-7	AIRTRAIN	20 MAR 98		21 MAR 98

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
 Client ID: 1-O-MM101A-FB
 Lab ID: 098186-0001-SA
 Matrix: AIRTRAIN
 Authorized: 21 MAR 98

Sampled: 20 MAR 98
 Prepared: See Below

Received: 21 MAR 98
 Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (3)	ND	ug/Sample	0.030	7471	24 MAR 98	24 MAR 98
Mercury, KCl (1&2)	0.33	ug/Sample	0.056	7471	24 MAR 98	24 MAR 98
Mercury, KMNO4	ND	ug/Sample	0.10	7471	23 MAR 98	23 MAR 98
Mercury, HCL	ND	ug/Sample	0.10	7471	24 MAR 98	24 MAR 98

ND = Not detected
 NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.

Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
 Client ID: Reagent Blanks
 Lab ID: 098186-0002-SA
 Matrix: AIRTRAIN
 Authorized: 21 MAR 98

Sampled: 20 MAR 98
 Prepared: See Below

Received: 21 MAR 98
 Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (1&2)	ND	ug/Sample	0.041	7471	24 MAR 98	24 MAR 98
Mercury, KMNO4	ND	ug/Sample	0.080	7471	23 MAR 98	23 MAR 98
Mercury, FH	ND	ug/sample	0.060	7471	24 MAR 98	24 MAR 98
Mercury, HCL	ND	ug/Sample	0.10	7471	24 MAR 98	24 MAR 98

ND = Not detected
 NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
 Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
 Client ID: 1-0-MM101A-4
 Lab ID: 098186-0003-SA
 Matrix: AIRTRAIN
 Authorized: 21 MAR 98

Sampled: 20 MAR 98
 Prepared: See Below

Received: 21 MAR 98
 Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (1&2)	24.7	ug/Sample	1.2	7471	24 MAR 98	24 MAR 98
Mercury, KCl (3)	0.30	ug/Sample	0.032	7471	24 MAR 98	24 MAR 98
Mercury, KMNO4	0.16	ug/Sample	0.10	7471	23 MAR 98	23 MAR 98
Mercury, HCL	ND	ug/Sample	0.10	7471	24 MAR 98	24 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
 NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
 Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-O-MM101A-5
Lab ID: 098186-0004-SA
Matrix: AIRTRAIN
Authorized: 21 MAR 98

Sampled: 20 MAR 98
Prepared: See Below

Received: 21 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (1&2)	17.3	ug/Sample	1.2	7471	24 MAR 98	24 MAR 98 o
Mercury, KCl (3)	0.21	ug/Sample	0.024	7471	24 MAR 98	24 MAR 98
Mercury, KMNO4	ND	ug/Sample	0.10	7471	23 MAR 98	23 MAR 98
Mercury, HCL	ND	ug/Sample	0.10	7471	24 MAR 98	24 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-O-MM101A-6
Lab ID: 098186-0005-SA
Matrix: AIRTRAIN
Authorized: 21 MAR 98

Sampled: 20 MAR 98
Prepared: See Below

Received: 21 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (1&2)	16.9	ug/Sample	1.1	7471	24 MAR 98	24 MAR 98 o
Mercury, KCl (3)	0.22	ug/Sample	0.039	7471	24 MAR 98	24 MAR 98
Mercury, KMNO4	ND	ug/Sample	0.10	7471	23 MAR 98	24 MAR 98
Mercury, HCL	ND	ug/Sample	0.10	7471	24 MAR 98	24 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-0-MM101A-7
Lab ID: 098186-0006-SA
Matrix: AIRTRAIN
Authorized: 21 MAR 98

Sampled: 20 MAR 98
Prepared: See Below

Received: 21 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (3)	0.33	ug/Sample	0.025	7471	24 MAR 98	25 MAR 98
Mercury, KCl (1&2)	26.4	ug/Sample	0.98	7471	24 MAR 98	24 MAR 98 o
Mercury, KMNO4	ND	ug/Sample	0.10	7471	23 MAR 98	24 MAR 98
Mercury, HCL	ND	ug/Sample	0.10	7471	24 MAR 98	24 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-I-MM101A-4
Lab ID: 098186-0007-SA
Matrix: AIRTRAIN
Authorized: 21 MAR 98

Sampled: 20 MAR 98
Prepared: See Below

Received: 21 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (1&2)	113	ug/Sample	3.6	7471	24 MAR 98	24 MAR 98 o
Mercury, KCl (3)	4.1	ug/Sample	0.26	7471	24 MAR 98	25 MAR 98 o
Mercury, KMNO4	3.0	ug/Sample	0.10	7471	23 MAR 98	24 MAR 98
Mercury, FH	33.3	ug/sample	1.2	7471	24 MAR 98	24 MAR 98 o
Mercury, HCL	0.20	ug/Sample	0.10	7471	24 MAR 98	24 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
 Client ID: 1-I-MM101A-5
 Lab ID: 098186-0008-SA
 Matrix: AIRTRAIN
 Authorized: 21 MAR 98

Sampled: 20 MAR 98
 Prepared: See Below

Received: 21 MAR 98
 Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (3)	0.46	ug/Sample	0.028	7471	24 MAR 98	25 MAR 98
Mercury, KCl (1&2)	48.6	ug/Sample	1.4	7471	24 MAR 98	24 MAR 98 o
Mercury, KMNO4	1.3	ug/Sample	0.10	7471	23 MAR 98	24 MAR 98
Mercury, FH	17.1	ug/sample	0.60	7471	24 MAR 98	24 MAR 98 o
Mercury, HCL	0.41	ug/Sample	0.10	7471	24 MAR 98	24 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
 NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
 Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
 Client ID: 1-I-MM101A-6
 Lab ID: 098186-0009-SA
 Matrix: AIRTRAIN
 Authorized: 21 MAR 98

Sampled: 20 MAR 98
 Prepared: See Below

Received: 21 MAR 98
 Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (1&2)	835	ug/Sample	39.0	7471	24 MAR 98	24 MAR 98 o
Mercury, KCl (3)	7.5	ug/Sample	0.28	7471	24 MAR 98	25 MAR 98 o
Mercury, KMNO4	3.2	ug/Sample	0.10	7471	23 MAR 98	24 MAR 98
Mercury, FH	98.0	ug/sample	6.0	7471	24 MAR 98	24 MAR 98 o
Mercury, HCL	0.92	ug/Sample	0.10	7471	24 MAR 98	24 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
 NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
 Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 1-I-MM101A-7
Lab ID: 098186-0010-SA
Matrix: AIRTRAIN
Authorized: 21 MAR 98

Sampled: 20 MAR 98
Prepared: See Below

Received: 21 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (3)	4.9	ug/Sample	0.26	7471	24 MAR 98	25 MAR 98 o
Mercury, KCl (1&2)	442	ug/Sample	16.0	7471	24 MAR 98	24 MAR 98 o
Mercury, KMNO4	4.6	ug/Sample	0.10	7471	23 MAR 98	24 MAR 98
Mercury, FH	38.9	ug/sample	1.2	7471	24 MAR 98	24 MAR 98 o
Mercury, HCL	0.96	ug/Sample	0.10	7471	24 MAR 98	24 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Barry Votaw

The cover letter is an integral part of this report.
Rev 230787

QC LOT ASSIGNMENT REPORT
Metals Analysis and Preparation

Laboratory Sample Number	QC Matrix	QC Category	QC Lot Number (DCS)	QC Run Number (LCS/BLANK)
098186-0001-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098186-0001-SA	AQUEOUS	HG-TRC-G	24 MAR 98-T	24 MAR 98-T
098186-0001-SA	AQUEOUS	HG-TRC-G	24 MAR 98-U	24 MAR 98-U
098186-0002-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098186-0002-SA	AQUEOUS	HG-TRC-G	24 MAR 98-T	24 MAR 98-T
098186-0002-SA	AQUEOUS	HG-TRC-G	24 MAR 98-U	24 MAR 98-U
098186-0003-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098186-0003-SA	AQUEOUS	HG-TRC-G	24 MAR 98-T	24 MAR 98-T
098186-0003-SA	AQUEOUS	HG-TRC-G	24 MAR 98-U	24 MAR 98-U
098186-0004-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098186-0004-SA	AQUEOUS	HG-TRC-G	24 MAR 98-T	24 MAR 98-T
098186-0004-SA	AQUEOUS	HG-TRC-G	24 MAR 98-U	24 MAR 98-U
098186-0005-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098186-0005-SA	AQUEOUS	HG-TRC-G	24 MAR 98-T	24 MAR 98-T
098186-0005-SA	AQUEOUS	HG-TRC-G	24 MAR 98-U	24 MAR 98-U
098186-0006-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098186-0006-SA	AQUEOUS	HG-TRC-G	24 MAR 98-T	24 MAR 98-T
098186-0006-SA	AQUEOUS	HG-TRC-G	24 MAR 98-U	24 MAR 98-U
098186-0007-MS	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098186-0007-MS	AQUEOUS	HG-TRC-G	24 MAR 98-T	24 MAR 98-T
098186-0007-MS	AQUEOUS	HG-TRC-G	24 MAR 98-U	24 MAR 98-U
098186-0007-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098186-0007-SA	AQUEOUS	HG-TRC-G	24 MAR 98-T	24 MAR 98-T
098186-0007-SA	AQUEOUS	HG-TRC-G	24 MAR 98-U	24 MAR 98-U
098186-0008-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098186-0008-SA	AQUEOUS	HG-TRC-G	24 MAR 98-T	24 MAR 98-T
098186-0008-SA	AQUEOUS	HG-TRC-G	24 MAR 98-U	24 MAR 98-U
098186-0009-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098186-0009-SA	AQUEOUS	HG-TRC-G	24 MAR 98-T	24 MAR 98-T
098186-0009-SA	AQUEOUS	HG-TRC-G	24 MAR 98-U	24 MAR 98-U
098186-0010-SA	AQUEOUS	HG-TRC-G	23 MAR 98-T	23 MAR 98-T
098186-0010-SA	AQUEOUS	HG-TRC-G	24 MAR 98-T	24 MAR 98-T
098186-0010-SA	AQUEOUS	HG-TRC-G	24 MAR 98-U	24 MAR 98-U

METHOD BLANK REPORT
Metals Analysis and Preparation
Project: 098186

Test: HG-CVAA-KMN04-AIRTRA Metals Emissions from Stationary Sources
Method: 7471
Matrix: AQUEOUS
QC Lot: 23 MAR 98-T

QC Run: 23 MAR 98-T

Analyte	Result	Units	Reporting Limit
Mercury, KMN04	ND	ug/L	0.20

Test: HG-CVAA-HCL-AIRTRAIN Metals Emissions From Stationary Sources
Method: 7471
Matrix: AQUEOUS
QC Lot: 24 MAR 98-T

QC Run: 24 MAR 98-T

Analyte	Result	Units	Reporting Limit
Mercury, HCL	ND	ug/L	0.20

Test: HG-CVAA-HCL-AIRTRAIN Metals Emissions From Stationary Sources
Method: 7471
Matrix: AQUEOUS
QC Lot: 24 MAR 98-T

QC Run: 24 MAR 98-T

Analyte	Result	Units	Reporting Limit
Mercury, FH	ND	ug/L	0.20

Test: HG-CVAA-KCL(1&2)-AIR Metals Emissions From Stationary Sources
Method: 7471
Matrix: AQUEOUS
QC Lot: 24 MAR 98-U

QC Run: 24 MAR 98-U

Analyte	Result	Units	Reporting Limit
Mercury, KCl (1&2)	ND	ug/L	0.20

ND = Not Detected

METHOD BLANK REPORT
Metals Analysis and Preparation
Project: 098186

(cont.)

Test: HG-CVAA-KCL(1&2)-AIR Metals Emissions From Stationary Sources
Method: 7471
Matrix: AQUEOUS
QC Lot: 24 MAR 98-U

QC Run: 24 MAR 98-U

Analyte	Result	Units	Reporting Limit
Mercury, KCl (3)	ND	ug/L	0.20

ND = Not Detected

DUPLICATE CONTROL SAMPLE REPORT
Metals Analysis and Preparation
Project: 098186

Category: HG-TRC-G Mercury analysis on air trains
Testcode: HG-CVAA-KMNO4-AIRTRA Method: 7471
Matrix: AQUEOUS Concentration Units: ug/L
QC Lot: 23 MAR 98-T Analyzed Date: 23 MAR 98 Time: 16:05

Analyte	-----Concentration-----			Accuracy		Precision	
	Spiked	-----Measured-----		Average(%)		(RPD)	
		DCS1	DCS2	AVG	DCS Limits	DCS Limit	
Mercury, KMNO4	1.00	0.969	0.972	0.970	97 80-120	0.3	20

Category: HG-TRC-G Mercury analysis on air trains
Testcode: HG-CVAA-HCL-AIRTRAIN Method: 7471
Matrix: AQUEOUS Concentration Units: ug/L
QC Lot: 24 MAR 98-T Analyzed Date: 24 MAR 98 Time: 14:15

Analyte	-----Concentration-----			Accuracy		Precision	
	Spiked	-----Measured-----		Average(%)		(RPD)	
		DCS1	DCS2	AVG	DCS Limits	DCS Limit	
Mercury, FH	1.00	0.984	1.02	1.00	100 80-120	3.8	20
Mercury, HCL	1.00	0.984	1.02	1.00	100 80-120	3.8	20

Category: HG-TRC-G Mercury analysis on air trains
Testcode: HG-CVAA-KCL(1&2)-AIR Method: 7471
Matrix: AQUEOUS Concentration Units: ug/L
QC Lot: 24 MAR 98-U Analyzed Date: 25 MAR 98 Time: 09:54

Analyte	-----Concentration-----			Accuracy		Precision	
	Spiked	-----Measured-----		Average(%)		(RPD)	
		DCS1	DCS2	AVG	DCS Limits	DCS Limit	
Mercury, KCL (1&2)	1.00	0.964	0.902	0.933	93 80-120	6.6	20
Mercury, KCL 3	1.00	0.964	0.902	0.933	93 80-120	6.6	20

MATRIX SPIKE / MATRIX SPIKE DUPLICATE REPORT
Metals Analysis and Preparation

Test: HG-CVAA-FH-AIRTRAIN
Sample: 098186-0007
Matrix: AIRTRAIN

Method: 7471
Sampled: 20 MAR 98
Units: ug/sample

Analyte	----- Concentration -----				Spiked		%Recovery		%
	Sample	Matrix Spike	Matrix Spike Dup	MS	MSD	MS	MSD	RPD	
Mercury, FH	33.3	33.9	NA	0.30		NC		NC	

NA = Not Applicable
NC = Not Calculated, calculation not applicable.

All calculations are performed before rounding to avoid round-off errors in calculated results.

MATRIX SPIKE / MATRIX SPIKE DUPLICATE REPORT
Metals Analysis and Preparation

Test: HG-CVAA-KCL(1&2)-AIR
Sample: 098186-0007
Matrix: AIRTRAIN

Method: 7471
Sampled: 20 MAR 98
Units: ug/Sample

Analyte	Sample	Concentration		Spiked		%Recovery		% RPD
		Matrix Spike	Matrix Spike Dup	MS	MSD	MS	MSD	
Mercury, KCl (1&2)	113	115	NA	0.36		NC		NC

NA = Not Applicable
NC = Not Calculated, calculation not applicable.

All calculations are performed before rounding to avoid round-off errors in calculated results.

MATRIX SPIKE / MATRIX SPIKE DUPLICATE REPORT
 Metals Analysis and Preparation

Test: HG-CVAA-KCL(3)-AIR
 Sample: 098186-0007
 Matrix: AIRTRAIN

Method: 7471
 Sampled: 20 MAR 98
 Units: ug/Sample

Analyte	----- Concentration -----			Spiked		%Recovery		
	Sample	Matrix Spike	Matrix Spike Dup	MS	MSD	MS	MSD	RPD
Mercury, KCl (3)	4.1	4.3	NA	0.13		NC		NC

NA = Not Applicable
 NC = Not Calculated, calculation not applicable.

All calculations are performed before rounding to avoid round-off errors in calculated results.

MATRIX SPIKE / MATRIX SPIKE DUPLICATE REPORT
Metals Analysis and Preparation

Test: HG-CVAA-KMNO4-AIRTRA
Sample: 098186-0007
Matrix: AIRTRAIN

Method: 7471
Sampled: 20 MAR 98
Units: ug/Sample

Analyte	----- Concentration -----			Spiked		%Recovery %		
	Sample	Matrix Spike	Matrix Spike Dup	MS	MSD	MS	MSD	RPD
Mercury, KMNO4	3.0	3.3	NA	0.50		NC		NC

NA = Not Applicable
NC = Not Calculated, calculation not applicable.

All calculations are performed before rounding to avoid round-off errors in calculated results.

MATRIX SPIKE / MATRIX SPIKE DUPLICATE REPORT
Metals Analysis and Preparation

Test: HG-CVAA-HCL-AIRTRAIN
Sample: 098186-0007
Matrix: AIRTRAIN

Method: 7471
Sampled: 20 MAR 98
Units: ug/Sample

Analyte	----- Concentration -----			Spiked		%Recovery		% RPD
	Sample	Matrix Spike	Matrix Spike Dup	MS	MSD	MS	MSD	
Mercury, HCL	0.20	0.70	NA	0.50		99		NC

NA = Not Applicable
NC = Not Calculated, calculation not applicable.

All calculations are performed before rounding to avoid round-off errors in calculated results.

AirKinetics, Inc.

EMISSIONS CHARACTERIZATION AND TESTING SERVICES

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 679-SG JOB NAME: Ogden - Lake

LABORATORY: Quanterra Environ. Services JOB No.: 10388

DATE SAMPLES WERE TRANSMITTED: 20-Mar-98 EXPECTED DATE OF RESULTS: 24-Mar-98

SAMPLE MATRIX: 0.1 N KCl, 4% KMnO4 / 10% H2SO4, 0.1N HNO3, 8N HCl

TYPE OF ANALYSIS REQUIRED: Please analyze according to EPA Method 101A for Hg.

Sample / Run ID #	Sample Collection Date	Sample Components	Sample Matrix	Condition of Samples *
1-O-MM101A-4	3/20/98	1st and 2nd Imp.	0.1N KCl	Preserved w/ KMnO4
		3rd Impinger	0.1N KCl	Preserved w/ KMnO4
		KMnO4	KMnO4/H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	
1-O-MM101A-5	3/20/98	1st and 2nd Imp.	0.1N KCl	Preserved w/ KMnO4
		3rd Impinger	0.1N KCl	Preserved w/ KMnO4
		KMnO4	KMnO4/H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	
1-O-MM101A-6	3/20/98	1st and 2nd Imp.	0.1N KCl	Preserved w/ KMnO4
		3rd Impinger	0.1N KCl	Preserved w/ KMnO4
		KMnO4	KMnO4/H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	
1-O-MM101A-7	3/20/98	1st and 2nd Imp.	0.1N KCl	Preserved w/ KMnO4
		3rd Impinger	0.1N KCl	Preserved w/ KMnO4
		KMnO4	KMnO4/H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: *[Signature]* Date/Time: 3/20/98

Transported by: FedEx Date/Time: _____

Transported to: Quanterra Environmental Services
880 Riverside Parkway
West Sacramento, CA 95605-1501

Received by: *[Signature]* Date/Time: 032198 14:05

5932 Bolsa Avenue, Suite 105 * Huntington Beach, CA 92649 * Phone (714) 373-0998 * Fax (714) 895-1915

Rec'd in good condition. 032198 mes

AirKinetics, Inc.

EMISSIONS CHARACTERIZATION AND TESTING SERVICES

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 679-SG JOB NAME: Ogden - Lake

LABORATORY: Quanterra Environ. Services JOB No.: 10388

DATE SAMPLES WERE TRANSMITTED: 20-Mar-98 EXPECTED DATE OF RESULTS: 24-Mar-98

SAMPLE MATRIX: 0.1 N KCl, 4% KMnO4 / 10% H2SO4, 0.1N HNO3, 8N HCl

TYPE OF ANALYSIS REQUIRED: Please analyze according to EPA Method 101A for Hg.

Sample / Run ID #	Sample Collection Date	Sample Components	Sample Matrix	Condition of Samples *
1-I-MM101A-4	3/20/98	1st and 2nd Imp.	0.1N KCl	Preserved w/ KMnO4
		3rd Impinger	0.1N KCl	Preserved w/ KMnO4
		KMnO4	KMnO4/H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	
		Filter	Filter	
		Front Half Rinse	0.1 N HNO3	
1-I-MM101A-5	3/20/98	1st and 2nd Imp.	0.1N KCl	Preserved w/ KMnO4
		3rd Impinger	0.1N KCl	Preserved w/ KMnO4
		KMnO4	KMnO4/H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	
		Filter	Filter	
		Front Half Rinse	0.1 N HNO3	

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: [Signature] Date/Time: 3/20/98

Transported by: FedEx Date/Time: _____

Transported to: Quanterra Environmental Services
880 Riverside Parkway
West Sacramento, CA 95605-1501

Received by: [Signature] Date/Time: 03/21/98 14:05

5932 Bolsa Avenue, Suite 105 * Huntington Beach, CA 92649 * Phone (714) 373-0998 * Fax (714) 898-1969

Rec'd in good condition 03/21/98 MP

AirKinetics, Inc.

EMISSIONS CHARACTERIZATION AND TESTING SERVICES

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 679-SG JOB NAME: Ogden - Lake

LABORATORY: Quanterra Environ. Services JOB No.: 10388

DATE SAMPLES WERE TRANSMITTED: 20-Mar-98 EXPECTED DATE OF RESULTS: 24-Mar-98

SAMPLE MATRIX: 0.1 N KCl, 4% KMnO4 / 10% H2SO4, 0.1N HNO3, 8N HCl

TYPE OF ANALYSIS REQUIRED: Please analyze according to EPA Method 101A for Hg.

Sample / Run ID #	Sample Collection Date	Sample Components	Sample Matrix	Condition of Samples *
1-I-MM101A-6	3/20/98	1st and 2nd Imp.	0.1N KCl	Preserved w/ KMnO4
		3rd Impinger	0.1N KCl	Preserved w/ KMnO4
		KMnO4	KMnO4/H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	
		Filter	Filter	
		Front Half Rinse	0.1 N HNO3	
1-I-MM101A-7	3/20/98	1st and 2nd Imp.	0.1N KCl	Preserved w/ KMnO4
		3rd Impinger	0.1N KCl	Preserved w/ KMnO4
		KMnO4	KMnO4/H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	
		Filter	Filter	
		Front Half Rinse	0.1 N HNO3	
* Sample spilled but is contained within the ziploc bag 032198				

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: SOCC Date/Time: 3/20/98

Transported by: FedEx Date/Time: _____

Transported to: Quanterra Environmental Services
880 Riverside Parkway
West Sacramento, CA 95605-1501

Received by: [Signature] Date/Time: 032198 14:05

Metals Emissions from Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 2-I-M101A-1
Lab ID: 098134-0002-SA
Matrix: AIRTRAIN
Authorized: 20 MAR 98

Sampled: 18 MAR 98
Prepared: See Below

Received: 19 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KMNO4	101	ug/Sample	4.0	7471	22 MAR 98	22 MAR 98 o
Mercury, HCL	4.2	ug/Sample	0.10	7471	23 MAR 98	23 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions from Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 2-0-M101A-1
Lab ID: 098134-0001-SA
Matrix: AIRTRAIN
Authorized: 20 MAR 98

Sampled: 18 MAR 98
Prepared: See Below

Received: 19 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KMNO4	7.7	ug/Sample	0.20	7471	22 MAR 98	22 MAR 98
Mercury, HCL	2.4	ug/Sample	0.10	7471	23 MAR 98	23 MAR 98

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 2-I-MM101A-1
Lab ID: 098134-0007-SA
Matrix: AIRTRAIN
Authorized: 20 MAR 98

Sampled: 18 MAR 98
Prepared: See Below

Received: 19 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (1&2)	110	ug/Sample	11.1	7471	22 MAR 98	22 MAR 98 o
Mercury, KCl (3)	0.33	ug/Sample	0.032	7471	21 MAR 98	22 MAR 98
Mercury, KMNO4	1.8	ug/Sample	0.20	7471	22 MAR 98	22 MAR 98
Mercury, FH	37.9	ug/sample	1.2	7471	22 MAR 98	22 MAR 98 o
Mercury, HCL	0.53	ug/Sample	0.10	7471	23 MAR 98	23 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
Rev 230787

Metals Emissions From Stationary Sources

Client Name: AirKinetics, Inc.
Client ID: 2-O-MM101A-1
Lab ID: 098134-0008-SA
Matrix: AIRTRAIN
Authorized: 20 MAR 98

Sampled: 18 MAR 98
Prepared: See Below

Received: 19 MAR 98
Analyzed: See Below

Parameter	Result	Units	Reporting Limit	Analytical Method	Prepared Date	Analyzed Date
Mercury, KCl (1&2)	7.4	ug/Sample	0.24	7471	22 MAR 98	22 MAR 98
Mercury, KCl (3)	0.048	ug/Sample	0.037	7471	21 MAR 98	22 MAR 98
Mercury, KMNO4	ND	ug/Sample	0.20	7471	22 MAR 98	22 MAR 98
Mercury, HCL	ND	ug/Sample	0.10	7471	23 MAR 98	23 MAR 98

Note o : Reporting limit(s) raised due to high level of analyte present in sample.

ND = Not detected
NA = Not applicable

Reported By: Marilyn Toomey

Approved By: Mei Lai

The cover letter is an integral part of this report.
Rev 230787

AirKinetics, Inc.

EMISSIONS CHARACTERIZATION AND TESTING SERVICES

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 679-56
~~646 GM~~ JOB NAME: Ogden - Lake

LABORATORY: Quanterra Environ. Services JOB No.: 10388

DATE SAMPLES WERE TRANSMITTED: 19-Mar-98 EXPECTED DATE OF RESULTS: 23-Mar-98

SAMPLE MATRIX: 4% KMnO4/10% H2SO4

TYPE OF ANALYSIS REQUIRED: Please analyze according to EPA Method 101A for Hg

Sample / Run ID #	Sample Collection Date	Sample Components	Sample Matrix	Condition of Samples *
2-O-M101A-1	3/18/98	KMnO4	KMnO4 / H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	
2-I-M101A-1	3/18/98	KMnO4	KMnO4 / H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: shcl Date/Time: 3/19/98

Transported by: FedEx Date/Time: _____

Transported to: Quanterra Environmental Services
880 Riverside Parkway
West Sacramento, CA 95605-1501

Received by: [Signature] Date/Time: 032098 1130

AirKinetics, Inc.

EMISSIONS CHARACTERIZATION AND TESTING SERVICES

REQUEST FOR ANALYSIS

PURCHASE ORDER No.: 679-SG

JOB NAME: Ogden - Lake

LABORATORY: Quanterra Environ. Services

JOB No.: 10327 10388

DATE SAMPLES WERE TRANSMITTED: 19-Mar-98

EXPECTED DATE OF RESULTS: _____

SAMPLE MATRIX: 0.1 N KCl, 4% KMnO4 / 10% H2SO4, 0.1N HNO3, 8N HCl

TYPE OF ANALYSIS REQUIRED: Please analyze according to EPA Method 101A for Hg only.

Sample / Run ID #	Sample Collection Date	Sample Components	Sample Matrix	Condition of Samples *
2-I-MM101A-1	3/18/98	Front Half Rinse	0.1N HNO3	
		Filter	Filter	
		1st and 2nd Imp.	0.1N KCl	Preserved with KMnO4
		3rd Impinger	0.1 N KCl	Preserved with KMnO4
		KMnO4	KMnO4 / H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	
2-O-MM101A-1	3/18/98	1st and 2nd Imp.	0.1 N KCl	Preserved with KMnO4
		3rd Impinger	0.1 N KCl	Preserved with KMnO4
		KMnO4	KMnO4 / H2SO4	
		8N HCl Rinse	8N HCl w/ DI H2O	

* For Laboratory Comments (temp., labels, etc.)

Samples Relinquished by: *clcc*

Date/Time: 3/19/98

Transported by: FedEx

Date/Time: _____

Transported to: Quanterra Environmental Services
880 Riverside Parkway
West Sacramento, CA 95605-1501

Received by: *McD...*

Date/Time: 032098 1120

APPENDIX D

ANALYTICAL DATA

3.0 CALSCIENCE ENVIRONMENTAL LABORATORIES, INC.

Calscience
Environmental
Laboratories, Inc.

April 03, 1998

Gary Mata
Air Kinetics, Inc.
5932 Bolsa Avenue, Suite 105
Huntington Beach, CA 92649

Subject: **Calscience Work Order Number: 98-03-904**
Client Reference: Ogden - Lake / 10388

Dear Client:

Enclosed is an analytical report for the above-referenced project. The samples included in this report were received 03/27/98 and analyzed in accordance with the attached chain-of-custody.

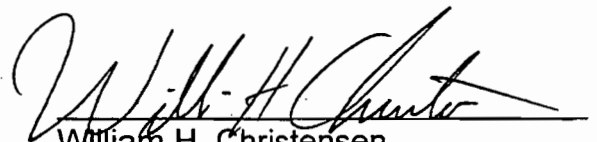
The results in this analytical report are limited to the samples tested, and any reproduction of this report must be made in its entirety.

If you have any questions regarding this report, require sampling supplies or field services, or information on our analytical services, please feel free to call me at (714) 895-5494.

Sincerely,



Calscience Environmental
Laboratories, Inc.
Jody McInerney
Project Manager



William H. Christensen
Deliverables Manager

D 78

Air Kinetics, Inc.
5932 Bolsa Avenue, Suite 105
Huntington Beach, CA 92649

Date Sampled: 03/20/98
Date Received: 03/27/98
Date Analyzed: 03/31/98

Attn: Gary Mata
RE: Ogden - Lake/10388

Work Order No.: 98-03-904
Method: EPA 26
Page 1 of 1

All concentrations are reported in µg/sample unless noted otherwise.

<u>Analyte</u>	<u>Concentration</u>	<u>Reporting Limit</u>
Sample Number: 1-O-M26-1 Impinger Contents		
HCl	44300	4730
Sample Number: 1-O-M26-1 Back Half		
Cl ₂	182	180
Sample Number: 1-O-M26-FB Impinger Contents		
HCl	ND	356
Sample Number: 1-O-M26-FB Back Half		
Cl ₂	ND	180
Sample Number: Method Blank		
Chloride	ND*	1

*Reported in mg/L (ppm).

ND denotes not detected at indicated reportable limit.

Each sample was received by CEL chilled, intact, and with chain-of-custody attached.

D 79

Air Kinetics, Inc.
 5932 Bolsa Avenue, Suite 105
 Huntington Beach, CA 92649

Date Sampled: 03/20/98
 Date Received: 03/27/98
 Date Digested: 03/30-31/98
 Date Analyzed: 03/30-04/02/98
 Work Order No.: 98-03-904

Attn: Gary Mata
 RE: Ogden - Lake/10388

Page 1 of 2

All concentrations are reported in mg/kg (ppm). Analyses for metals were conducted on a total digestion.

<u>Analyte</u>	<u>Method</u>	<u>Concentration</u>	<u>Reporting Limit</u>
Sample Number: ASH-1			
Mercury	EPA 7471A	12.3	2.5
Mercury(KCl extract)	EPA 7471A	ND	0.25
Selenium	EPA 6010A	ND	2.0
Titanium	EPA 6010A	984	2.0
Vanadium	EPA 6010A	17	2.0
Calcium	EPA 6010A	168000	1000
Sample Number: ASH-2			
Mercury	EPA 7471A	18.4	5.0
Mercury(KCl extract)	EPA 7471A	ND	0.25
Selenium	EPA 6010A	ND	2.0
Titanium	EPA 6010A	742	2.0
Vanadium	EPA 6010A	14	2.0
Calcium	EPA 6010A	162000	1000
Sample Number: Method Blank			
Mercury	EPA 7471A	ND	0.25
Mercury(KCl extract)	EPA 7471A	ND	0.25
Selenium	EPA 6010A	ND	1.0
Titanium	EPA 6010A	ND	1.0
Vanadium	EPA 6010A	ND	1.0
Calcium	EPA 6010A	ND	5.0

ND denotes not detected at indicated reportable limit.

Each sample was received by CEL chilled, intact, and with chain-of-custody attached. D 80

Air Kinetics, Inc.
5932 Bolsa Avenue, Suite 105
Huntington Beach, CA 92649

Date Sampled: 03/20/98
Date Received: 03/27/98
Date Analyzed: 04/02/98

Attn: Gary Mata
RE: Ogden - Lake/10388

Work Order No.: 98-03-904
Method: EPA 9038
Page 1 of 1

All concentrations are reported in mg/kg (ppm).

<u>Sample Number</u>	<u>Sulfate Concentration</u>	<u>Reporting Limit</u>
ASH-1	9600	1000
ASH-2	9500	1000
Method Blank	ND	10

ND denotes not detected at indicated reportable limit.

Each sample was received by CEL chilled, intact, and with chain-of-custody attached.

ANALYTICAL REPORT

Air Kinetics, Inc.
 5932 Bolsa Avenue, Suite 105
 Huntington Beach, CA 92649

Date Sampled: 03/20/98
 Date Received: 03/27/98
 Date Analyzed: 04/02/98

Attn: Gary Mata
 RE: Ogden - Lake/10388

Work Order No.: 98-03-904
 Method: SM 4500 Cl-C
 Page 1 of 1

All concentrations are reported in mg/kg (ppm).

<u>Sample Number</u>	<u>Chloride Concentration</u>	<u>Reporting Limit</u>
ASH-1	330000	20000
ASH-2	330000	20000
Method Blank	ND	10

ND denotes not detected at indicated reportable limit.

Each sample was received by CEL chilled, intact, and with chain-of-custody attached.

D 82

ANALYTICAL REPORT

Air Kinetics, Inc.
5932 Bolsa Avenue, Suite 105
Huntington Beach, CA 92649

Date Sampled: 03/20/98
Date Received: 03/27/98
Date Analyzed: 04/02/98

Attn: Gary Mata
RE: Ogden - Lake/10388

Work Order No.: 98-03-904
Method: EPA 340.2
Page 1 of 1

All concentrations are reported in mg/kg (ppm).

<u>Sample Number</u>	<u>Fluoride Concentration</u>	<u>Reporting Limit</u>
ASH-1	34.7	1.0
ASH-2	38.3	1.0
Method Blank	ND	0.5

ND denotes not detected at indicated reportable limit.

Each sample was received by CEL chilled, intact, and with chain-of-custody attached.

D 83



CORE LABORATORIES
ANALYTICAL REPORT
Job Number: 980395
Prepared For:
Calscience Environmental Labs, Inc
Jody Mc Inerney
7440 Lincoln Way
Garden Grove, CA 92841-1432
Date: 04/02/98

Signature 

Date: 4/2/98

Name: Greg L. Cook

Core Laboratories-Carson
21730 S. Wilmington Suite 201
Carson, CA 90810

Title: Supervising Chemist



LABORATORY TESTS RESULTS
04/02/98

JOB NUMBER: 980395 CUSTOMER: Calscience Environmental Labs, Inc ATIN: Jody Mc Inerney

CLIENT I.D.: Ash-1, 98-03-904
DATE SAMPLED: 03/20/98
TIME SAMPLED: 00:00
WORK DESCRIPTION: Ash-1, 98-03-904

LABORATORY I.D.: 980395-0001
DATE RECEIVED: 03/30/98
TIME RECEIVED: 15:45
REMARKS: 4oz. Plastic Cup

TEST DESCRIPTION	FINAL RESULT	LIMITS/*DILUTION	UNITS OF MEASURE	TEST METHOD	DATE	TECHN
C, H, N		*1		ASTM D-5291	04/02/98	QTI
Carbon Content	1.28	0.05	% Wt.	Carlo Erba		
Hydrogen Content	1.18	0.05	% Wt.	Carlo Erba		
Nitrogen Content	<0.05	0.05	% Wt.	Carlo Erba		

21730 S. Wilmington Suite 201
Carson, CA 90810
(310) 513-2031

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CORE LABORATORIES

LABORATORY TESTS RESULTS
04/02/98

JOB NUMBER: 980395 CUSTOMER: Calscience Environmental Labs, Inc ATTN: Jody Mc Inerney

CLIENT I.D.....: Ash-2, 98-03-904
DATE SAMPLED.....: 03/20/98
TIME SAMPLED.....: 00:00
WORK DESCRIPTION...: Ash-2, 98-03-904

LABORATORY I.D....: 980395-0002
DATE RECEIVED....: 03/30/98
TIME RECEIVED....: 15:45
REMARKS.....: 4oz. Plastic Cup

TEST DESCRIPTION	FINAL RESULT	LIMITS/*DILUTION	UNITS OF MEASURE	TEST METHOD	DATE	TECHN
C, H, N		*1		ASTM D-5291	04/02/98	QTI
Carbon Content	1.58	0.05	% Wt.	Carlo Erba		
Hydrogen Content	0.96	0.05	% Wt.	Carlo Erba		
Nitrogen Content	<0.05	0.05	% Wt.	Carlo Erba		

21730 S. Wilmington Suite 201
Carson, CA 90810
(310) 513-2031

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40 Lane Road
Fairfield, NJ 07007
973 882 9000
Fax 973 882 4156

SOURCE TEST PLAN - OEG Report No. 2256

April 6, 1998

Source Information

Facility: Ogden Martin Systems of Lake, Inc.
3830 Rogers Industrial Park
P.O. Box 189
Okahumpka, FL 34762

Purpose of Test: Demonstration of Compliance with Florida Department of
Environmental Protection, Permit/Certification No. AO35-
193817, PSD-FL-113 and Rule 62-296.

Person(s) to Contact: Mr. Cecil Boatwright, Facility Manager
(904) 365-1611

Mr. G. J. Aldina
Sr. Vice President, Environmental Testing/CEM
(973) 882-4136

Testing Firm Information

Company: Air Kinetics, Inc.

Testing Information **Option 2**

Procedure: Testing Unit 1 for mercury and Unit 2 for various air
pollutant emissions. Units 1 and 2 will be tested while firing
co-mingled biohazardous waste with MSW.

Proposed Test Dates: April 21-23, 1998

Prepared by: Jacqueline D. Heard

TABLE OF CONTENTS

<u>SECTION</u>	<u>PAGE</u>
1.0 INTRODUCTION	1
2.0 SCHEDULE OF ACTIVITIES	4
3.0 QUALITY ASSURANCE / QUALITY CONTROL.....	5
4.0 SOURCE TEST INFORMATION	
4.1 Description of Operation.....	6
4.2 Testing Platform Diagram	8
5.0 OPERATIONAL PARAMETERS	10

APPENDIX A: OPERATOR CERTIFICATION DOCUMENTS

APPENDIX B: PERMIT CONDITIONS

1.0 INTRODUCTION

A contractor for Ogden Martin Systems of Lake, Inc., will test the following air pollutant emissions from the Lake County Resource Recovery Facility for determination of compliance with Florida Department of Environmental Protection, Permit/Certification No. AO35-193817, PSD-FL-113 and Rule 62-296. Biohazardous waste will be charged to Unit 1 and Unit 2 during testing.

- (1) Biohazardous waste containers (boxes) will be weighed before being placed on the inclined conveyor for transport to the charging hopper. An operator at the hopper charging level will be in radio contact with tipping floor and control room operators to ensure mixing of MSW and the biohazardous waste.

Charging of the biohazardous waste to the charging hopper shall commence at least 30 minutes before initiating the EPA test procedures. This staging approach is to ensure that flue gas characteristics during the test period represents the co-mingled waste streams.

1.0 INTRODUCTION - CONT'D

Table 1-1: Emission Test Procedures

Pollutant	Permit Condition	Reference Sampling Method	Unit No.	Replicates	Approximate Sampling Time (Minutes)
Particulate Matter (PM)	8a	U.S. EPA Method 5	Unit 2	1, 2, 3	120
Oxides of Nitrogen (NO _x)	8a	U.S. EPA Method 7E	Unit 2	1, 2, 3	60
Carbon Monoxide (CO)	8a	U.S. EPA Method 10	Unit 2	1, 2, 3	60
Visible Emissions (VE)	8b	U.S. EPA Method 9	Unit 2	1, 2, 3	60
Hydrogen Chloride (HCl) ⁽¹⁾	8a	U.S. EPA Method 26	Unit 2	1, 2, 3	120
Sulfur Dioxide (SO ₂) ⁽¹⁾	8d	U.S. EPA Method 6C	Unit 2	1, 2, 3	60
Mercury (Hg) ⁽¹⁾	Rule 62-296	U.S. EPA Method 29	Unit 1,2	1, 2, 3	120
Oxygen/Carbon Dioxide (O ₂ / CO ₂)		U.S. EPA Method 3/3A	Unit 1,2	1, 2, 3 ⁽²⁾

⁽¹⁾ SO₂, HCl and Hg will be sampled at the inlet and outlet of the air pollution control equipment.

⁽²⁾ Oxygen/Carbon Dioxide will be tested concurrently with each pollutant except visible emissions.

2.0 SCHEDULE OF ACTIVITIES

2.0 SCHEDULE OF ACTIVITIES ⁽¹⁾

Day	Unit	Parameter ⁽²⁾	Reference Method	Replicates
0	-----	Setup		
1 ⁽³⁾	1	Hg ⁽⁴⁾	EPA 29	1, 2, 3
2 ⁽³⁾	2	Hg ⁽⁴⁾	EPA 29	1, 2, 3
3 ⁽³⁾	2	PM/HCl ⁽⁴⁾	EPA 5/26	1, 2, 3
	2	VE ⁽⁵⁾	EPA 9	1, 2, 3
	2	SO ₂ ⁽⁴⁾ , NO _x , CO	EPA 6C, 7E, 10	1, 2, 3

⁽¹⁾ Schedule may change during the testing to accommodate site conditions.

⁽²⁾ Emission tests will be conducted simultaneously for all pollutants except Hg.

⁽³⁾ This test day is designated for evaluating the combustion of biohazardous waste with MSW. Biohazardous waste will be weighed prior to addition to the boiler feed bypass. Feedrate will be greater than or equal to 10% of total feed to this boiler.

⁽⁴⁾ SO₂, HCl and Hg will be sampled at the inlet and outlet of the air pollution control equipment. HCL will be sampled for 120 minutes simultaneously during each PM test.

⁽⁵⁾ VE observations will be conducted for 60 minutes simultaneously during each PM test.

3.0 QUALITY ASSURANCE / QUALITY CONTROL

3.0 QUALITY ASSURANCE / QUALITY CONTROL

Ogden Energy Group, Inc. (OEG) has instituted a rigorous Quality Assurance/Quality Control (QA-QC) program for all of its air pollution testing. This program ensures that the emission data reported for OEG facilities are as accurate and meaningful as possible.

Glass or Teflon is employed in all of the sampling equipment in contact with the sample gas. This includes the nozzle, probe liner, filter housing, sample line and impingers. Calibration of all gas meters, thermocouples, and pitot tubes used in the test program will be performed using reference methods with calibration sheets included in the final report.

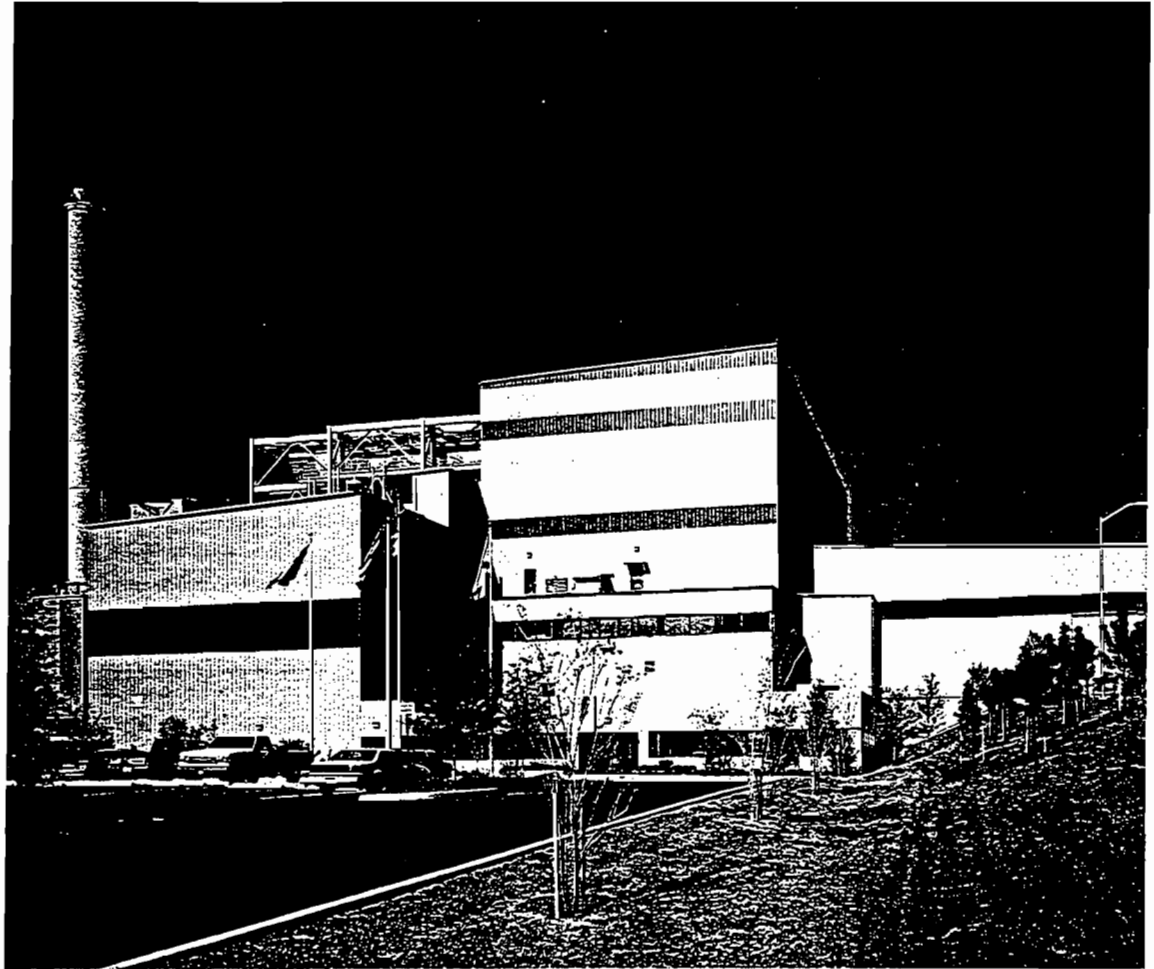
Transportation blanks, method blanks, inert sample containers, field data and chain of custody forms from the U.S. EPA QA Handbook for Air Pollution Measurement Systems, Volume III, Stationary Source Specification Methods, EPA-600/4-77-027b, are used during all phases of the test program.

All test programs include a supervising engineer from OEG's Fairfield, New Jersey, office to ensure the integrity of the test program according to the Source Test Plan.

4.0 SOURCE TEST INFORMATION

OGDEN MARTIN SYSTEMS OF LAKE, INC.

4.1 DESCRIPTION OF OPERATION



The Lake County
Resource Recovery
Facility

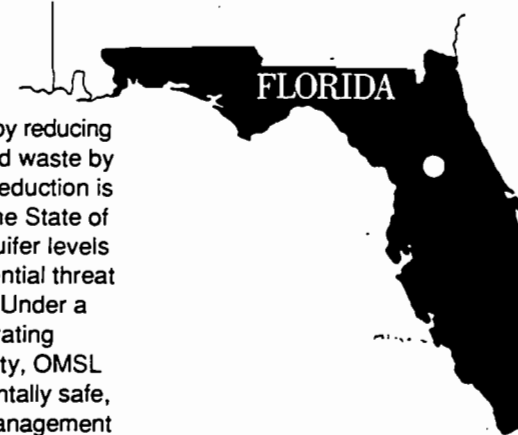
THE LAKE COUNTY RESOURCE RECOVERY FACILITY

THE LAKE COUNTY RESOURCE RECOVERY FACILITY

The Lake County Resource Recovery Facility, which began commercial operation in March, 1991, processes up to 528 tons of solid waste each day, generating up to 14.5 megawatts of electricity. The facility runs on approximately two megawatts of the energy it produces; the remainder is sold to a local utility and used to power area homes and businesses. Energy production reduces the amount of coal and oil burned by the power company, thus protecting the environment from related emissions. In addition, the County retains 90% of energy sales revenues which helps offset

project costs.

Designed, built, owned and operated by Ogden Martin Systems of Lake, Inc. (OMSL), the facility helps save valuable landfill space by reducing the volume of delivered waste by 90%. This significant reduction is of particular value in the State of Florida where high aquifer levels make landfilling a potential threat to groundwater purity. Under a twenty-three year operating contract with the County, OMSL will provide environmentally safe, effective solid waste management services to County residents well into the future.



RECYCLING WASTE INTO ENERGY

The facility's mass burn combustion system incorporates the technology of German-based Martin GmbH. Waste is combusted at furnace temperatures exceeding 1,800 degrees Fahrenheit and reduced to an

inert ash residue which is approximately 10% of the original volume of delivered waste. Before leaving the facility, combustion air is directed through technologically advanced air pollution control equipment consisting of dry flue

gas scrubbers and fabric filter baghouses. Facility emissions are strictly regulated by state and federal agencies, as are handling and disposal of combustion ash.

AN INTEGRATED SOLUTION

The resource recovery facility anchors an integrated solid waste management system which includes recycling via City- and County-sponsored curbside collection programs, private buy-back centers and County-run drop-off centers. Materials recycled include plastic and glass containers, aluminum cans and

newspapers. In addition, the County encourages citizens to deposit batteries in collection buckets placed at retail outlets and public buildings and operates a permanent household hazardous waste collection center—one of the first in Florida. In addition, ferrous metal recovered from combustion ash is a major

contributor to local recycling efforts.

The Lake County Resource Recovery Facility is located in Okahumpka, about 55 miles northwest of Orlando. For information or to arrange a tour, please call 904-365-1611.

FACILITY SPECIFICATIONS

Rated Refuse Combustion Capacity
528 tons per day

Unit Design
Two 264 ton per day waterwall furnaces

Guaranteed Throughput
163,000 tons per year

Guaranteed Waste Delivery
130,000 tons per year

Energy Generation at Rated Capacity
Up to 14.5 MW, sold to Florida Power Corporation

OGDEN MARTIN SYSTEMS OF LAKE, INC.

3830 Rogers Industrial Park Road
PO Box 189
Okahumpka, Florida 34762



4.2 SAMPLING AREA DESCRIPTION

The sampling points for the performance of the test program are at the sampling platform, 80 feet above the grade on the main stack (sampling ports are at an elevation of 85 feet). There are three flues, each with an inside diameter of 5 feet, 3 inches. Each flue has two sampling ports, 90 degrees apart and 6 inches in diameter. These sampling ports are located greater than 8 diameters after a disturbance and greater than 8 diameters before the stack outlet.

5.0 OPERATIONAL PARAMETERS

5.0 OPERATIONAL PARAMETERS

During the air pollutant emissions testing, plant process data will be monitored and collected by OMS personnel to ensure representative operation of the facility. Steam flow rate will be used to document facility capacity and firing rate.

APPENDIX A: OPERATOR CERTIFICATION DOCUMENTS

OPERATOR CERTIFICATION DOCUMENTS

Enclosed are the certification sheets that state the operators are trained in the operation of a biomedical incinerator. The certifications are enclosed in compliance with Rule DER 62-296.401(4)(e)10.

Certified Biomedical Incinerator Operator

This is to Certify that

JOHN FERGUSON

met the specifications of the Florida
Administrative Code, Rule 17-296.401
(4) (e) during training and test-
ing conducted by Biomedical Training
and Consulting, Inc. of Plant City,
Florida.

Herald Q. Daniels
President

211-9-93

Certificate
Number

9-25-93

OSBEN MARTEN

Date of Training.

Location

Certified Biomedical Incinerator Operator

This is to Certify that

MICHAEL M. DANIEL

met the specifications of the Florida
Administrative Code, Rule 17-296.401
(4) (e) during training and test-
ing conducted by Biomedical Training
and Consulting, Inc. of Plant City,
Florida.

Herald A. Daniels
President

212-9-93

Certificate
Number

9-25-93

OBEN MARTIN

Date of Training

Location

Certified Biomedical Incinerator Operator

This is to Certify that

PHILIP HOOP

met the specifications of the Florida
Administrative Code, Rule 17-296.401
(4) (e) during training and test-
ing conducted by Biomedical Training
and Consulting, Inc. of Plant City,
Florida.

Harold G. Evans
President

213-9-93

Certificate
Number

9-25-93

GIBEN MARTIN

Date of Training

Location

Certified Biomedical Incinerator Operator

This is to Certify that

CECIL BOATWRIGHT

*met the specifications of the Florida Administrative Code,
Part VI, 17-2.600 (1) (d) 4.g during training and testing
conducted by Biomedical Training And Consulting, Inc. of
Tampa, Florida.*

Gerald Durando

President

ZURIN
INDUSTRIAL INCINERATORS

Equipment Manufacturer

101294 AND 101295

Serial Number

92007

Certificate Number

JANUARY 29, 1992

Date of Training

3030 ROGERS INDUSTRIAL
PARK ROAD

OKAHUMPKA, FLORIDA

Location

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Certified Biomedical Incinerator Operator

This is to Certify that

DAVID [unclear]

met the specifications of the Florida Administrative Code,
Part VI, 17-2.600 (1) (d) 4.g during training and testing
conducted by Biomedical Training And Consulting, Inc. of
Tampa, Florida.

David [unclear]

President

ZURIX
INDUSTRIAL INCINERATORS

Equipment Manufacturer

101294 AND 101295

Serial Number

92002

Certificate Number

JANUARY 29, 1992

Date of Training

1010 ROUTE 2 INDUSTRIAL
PAGE 20110

TAMPA, FLORIDA

Location

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Certified Biomedical Incinerator Operator

This is to Certify that

TOM MURPHY

met the specifications of the Florida Administrative Code,
Part VI, 17-2.600 (1) (d) 4.g during training and testing
conducted by Biomedical Training And Consulting, Inc. of
Tampa, Florida.

Michael Dennis

President

ZURIX
INDUSTRIAL INCINERATORS

Equipment Manufacturer

101294 AND 101295

Serial Number

92005

Certificate Number

JANUARY 29, 1997

Date of Training
1010 ROGERS INDUSTRIAL
PARK ROAD
OKAUCHEEA, FLORIDA

Location

APPENDIX B: PERMIT CONDITIONS

G.J. ALDINA,
Senior Vice President
Environmental Testing/CEM

40 Lane Road CN 2615
Fairfield, NJ 07007-2615
973 882 4136
Fax 973 882 4156

12 March 1999

Mr. Gary Kuberski
Florida Department of Environmental Protection
Air Division, Central District Office
3319 Maguire Blvd., Suite 232
Orlando, Florida 32803

*Subject: OMS Lake, Inc.
OEG Report No.2373
Compliance Testing Results*

Dear Mr. Kuberski:

Enclosed, please find the results of the annual emission testing and relative accuracy test audit (RATA) conducted at Ogden Martin Systems of Lake, Inc. facility on 26-29 January 1999. All testing was done in accordance with the source test plan submitted prior to testing.

The results of these tests successfully demonstrated compliance with the permit A035-193817, Specific Condition 8 and Florida Rule 62-296.416 (3) (a) 1, emission limits for particulate matter, opacity, hydrogen chloride and sulfur dioxide from Units 1 and 2. Mr Jason Gorrie, the environmental engineer for the Lake facility, had a telecon with you on 17 February 1999 concerning preliminary indications that the mercury emission results for both units were unusual. The results for the 26 January mercury testing did not satisfactorily demonstrate compliance with the emissions limits imposed at 62-296.416, F.A.C. The Unit 1 mercury emission results indicated concentrations that were well outside the known database for any WTE facility. The results for Unit 2 did not demonstrate compliance with the emission limit.

These test results represented a confusing anomaly given the number of successful mercury compliance tests conducted at this facility dating back to the installation of the carbon injection system in 1995. It appeared that the carbon injection system was functional during this test program. Routine inspection of the carbon system during the tests did not immediately identify operational problems with the system. The Unit 2 system required maintenance shortly after the completion of the compliance test program; the drive belt for the injection system required replacement.

Immediate and determined efforts were initiated to investigate these unsatisfactory and confusing events. The emission test contractor was brought back to the facility to collect additional

Letter to G. Kuberski
12 March 1999
Page 2

mercury emission data. The results of that sampling event provide clear evidence that the the facility Unit 1 and 2 are in compliance with mercury emissions limitations.

The Unit 2 carbon system maintenance was successful in returning it to compliance. The anomalous results for Unit 1 are not indicative of normal operation and compliance with emission standards. In order to formally demonstrate compliance, we propose to retest both units using USEPA Method 29 on or about the week of 19 April 1999. We will be transmitting a Source Test Plan to you under separate cover.

We are prepared to meet with you at your earliest convenience to discuss the results of these tests. Please call me to arrange this meeting.

Sincerely,



G. J. Aldina
Sr. Vice President
Environmental Testing/CEM

GJA:kr

cc: S. Bass
C. Boatwright
G. Crane
B. Goldate
J. Gorrie
N. Gorsky
J. Klett
G. Main
D. Porter
Z. Semanyshyn
M. Slaby
N. Tammi

40 Lane Road
Fairfield, NJ 07007
973 882 9000
Fax 973 882 4156

ENVIRONMENTAL TEST REPORT

VOLUME 1

EXECUTIVE SUMMARY - OEG REPORT NO. 2373R

MARCH 26, 1999

PREPARED FOR: Ogden Martin Systems of Lake, Inc.
3830 Rogers Industrial Park
P. O. Box 189
Okahumpka, Florida 34762

PURPOSE: To Demonstrate Compliance with Florida Department of
Environmental Protection, Permit No. AO35-193817 and
Rule 62-296.

TEST DATES: January 26-29, 1999

ASSOCIATED REPORTS: OEG Report No. 2330

PREPARED BY: Ogden Energy Group, Inc.
Department 38 - CEM/Emission Testing

TABLE OF CONTENTS

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VOLUME 2: Testar, Inc. Report on Compliance Testing
(Bound Separately)

VOLUME 3: Confidential Process Data
(Bound Separately)

1.0 INTRODUCTION

Ogden Martin System of Lake, Inc. (OMSL) performed compliance emission tests at the Lake County Resource Recovery Facility from January 26-29, 1999. The purpose of this test program was to demonstrate compliance with the Florida Department of Environmental Protection (FLDEP), Permit No. AO35-193817, Specific Condition 8 and Rule 62-296. The testing was performed by Testar, Inc. in accordance with all procedures in the FLDEP approved test protocol.

The OMSL municipal solid waste combustion facility is located in Okahumpka, FL. The facility is rated at 528 tons of municipal solid waste per day. Units 1 and 2 were tested for mercury emissions at the economizer outlet and stack. Acid gas emissions were tested at the inlet and outlet of the air pollution control equipment. All testing was conducted simultaneously in accordance with procedures required by Florida Department of Environmental Protection (FLDEP) regional office.

A summary of emission test results for the facility is presented in Section 2.0, Tables 2.1 and 2.2. The Testar report (Volume 2) includes all testing data gathered at the site and all laboratory analytical data.

The test program, as indicated in the Source Test Plan (OEG Report No. 2330), is presented in Section 3.0, Table 3.2. Test observers and participants are presented in Table 3.1. The Schedule of Activities is presented in Table 3.3.

The mercury emission data for both units are not consistent with the control efficiency expected with activated carbon injection systems. The carbon injection system at the facility operated in accordance with permit requirements at all times without malfunction. The laboratory analysis for mercury was conducted twice. The results of the second analysis appear in the following tables. The results from the original analysis can be found in the appendices of Testar's report, Volume 2.

2.0 SUMMARY OF RESULTS

TABLE 2.1
SUMMARY OF SOURCE TEST RESULTS - UNIT 1

Pollutant	----- Replicate ⁽¹⁾ -----			Average	Permitted Compliance Emission Limits
	1	2	3		
<u>SDA INLET</u>					
<u>Conc., ppmdv @ 7% O₂</u> Hydrogen Chloride (HCl)	1486	1298	1217	1334	-----
<u>Conc., ppmdv @ 12% CO₂</u> Sulfur Dioxide (SO ₂)	42.5	24.7	25.1	30.8	-----
<u>Conc., ug/DSCM @ 7% O₂</u> Mercury (Hg)	9278	5595	699	5191	-----
<u>STACK ⁽²⁾</u>					
<u>Conc., ppmdv @ 7% O₂</u> Hydrogen Chloride (HCl)	29.9	27.6	33.2	30.2	50
Carbon Monoxide (CO)	16.7	13.6	18.4	16.2	100
<u>Conc., ppmdv @ 12% CO₂</u> Sulfur Dioxide (SO ₂)	6.46	3.65	3.04	4.38	60
Nitrogen Oxides (NO _x)	264	271	304	280	385
<u>Conc., gr/dscf @ 7% O₂</u> Particulate Matter (PM)	0.0131	0.00472	0.00595	0.00792	0.02
<u>Conc., gr/dscf @ 12% CO₂</u> Particulate Matter (PM)	0.0128	0.00487	0.00600	0.00789	0.015
Mercury (Hg)	2.93E-03	6.49E-04	2.98E-04	1.29E-03	3.4E-04
<u>Conc., ug/dscm @ 7% O₂</u> Mercury (Hg)	6787	1503	693	2994	-----
<u>Emission Rate, lb/hr</u> Mercury (Hg)	0.610	0.155	0.0637	0.276	-----
Particulate (PM)	2.90	1.06	1.29	1.75	-----
<u>Removal Efficiency, %</u> Hydrogen Chloride (HCl) ⁽³⁾	98.0	97.9	97.3	97.7	≥90
Mercury (Hg) ⁽³⁾	26.9	73.1	0.9	33.6	≥80
Sulfur Dioxide (SO ₂) ⁽⁴⁾	84.8	85.2	87.9	86.0	≥70
<u>Opacity, %</u> Visible Emissions (VE)	0	0	0	0	15

⁽¹⁾ Data presented as repetition number. Actual sample run number may differ.

⁽²⁾ All testing for HCl, SO₂, NO_x, CO, opacity, and particulate done simultaneously.

⁽³⁾ Based on lb/hr.

⁽⁴⁾ Based on ppmdv @ 7% O₂.

TABLE 2.2
SUMMARY OF SOURCE TEST RESULTS - UNIT 2

Pollutant	----- Replicate -----			Average	Permitted Compliance Emission Limits
	1	2	3		
<u>SDA INLET</u>					
<u>Conc., ppmdv @ 7% O₂</u> Hydrogen Chloride (HCl)	687	710	800	732	-----
<u>Conc., ppmdv @ 12% CO₂</u> Sulfur Dioxide (SO ₂)	25.6	11.9	15.8	17.8	-----
<u>Conc., ug/DSCM @ 7% O₂</u> Mercury (HCl)	1068	693	281	681	-----
<u>STACK ⁽¹⁾</u>					
<u>Conc., ppmdv @ 7% O₂</u> Hydrogen Chloride (HCl)	17.9	7.88	19.3	15.0	50
Carbon Monoxide (CO)	31.6	21.4	19.1	24.0	100
<u>Conc., ppmdv @ 12% CO₂</u> Sulfur Dioxide (SO ₂)	0.565	0.000	0.698	0.421	60
Nitrogen Oxides (NOx)	265	334	345	315	385
<u>Conc., gr/dscf @ 7% O₂</u> Particulate Matter (PM)	0.00468	0.00343	0.00393	0.00401	0.020
<u>Conc., gr/dscf @ 12% CO₂</u> Particulate Matter (PM)	0.00464	0.00339	0.00392	0.00398	0.015
Mercury (Hg)	2.27E-04	6.64E-05	4.19E-05	1.12E-04	3.4E-04
<u>Conc., ug/dscm @ 7% O₂</u> Mercury (Hg)	520	155	97.3	258	-----
<u>Emission Rate, lb/hr</u> Mercury (Hg)	0.0461	0.0144	0.00935	0.0233	-----
Particulate (PM)	0.995	0.742	0.794	0.844	-----
<u>Removal Efficiency, %</u> Sulfur Dioxide (SO ₂) ⁽²⁾	97.8	100	95.6	97.8	≥70
Hydrogen Chloride (HCl) ⁽³⁾	97.4	98.9	97.6	98.0	≥90
Mercury (Hg) ⁽³⁾	52.0	78.1	65.3	65.1	≥80
<u>Opacity, %</u> Visible Emissions (VE)	0	0	0	0	15

⁽¹⁾ All testing for HCl, SO₂, NOx, CO, opacity, and particulate done simultaneously.

⁽²⁾ Based on ppmvd @ 7% CO₂.

⁽³⁾ Based on lb/hr.

3.0 TEST PROGRAM

TABLE 3.1
TEST PARTICIPANTS

Ogden Energy Group, Inc.

G. J. Aldina

Testar, Inc.

Gary Williams
David Brintle
Herb Dixon
Joe Daley
Bill Harris
Dan Beatty

Malcolm Pirnie

John Pacifici
Chip Gerlock

TABLE 3.2
TEST PROGRAM

Parameter	Method
Particulate Matter (PM)	U.S. EPA Method 5
Sulfur Dioxide (SO ₂) ⁽¹⁾	U.S. EPA Method 6C
Nitrogen Oxides (NO _x)	U.S. EPA Method 7E
Carbon Monoxide (CO)	U.S. EPA Method 10
Visible Emissions (VE)	U.S. EPA Method 9
Hydrogen Chloride (HCl) ⁽¹⁾	U.S. EPA Method 26
Mercury (Hg) ⁽¹⁾	U.S. EPA Method 29

⁽¹⁾ SO₂, HCl and Hg sampled at the inlet and outlet of the air pollution control equipment.

TABLE 3.3
SCHEDULE OF ACTIVITIES

Date/ Time	Unit	Location	Sampling Method	Replicate (Run)	Parameter
<u>1/26/99</u>					
0836-1045	1	Outlet	EPA 5/26	1	PM/HCl
0842-1042	1	Inlet	EPA 26	1	HCl
0844-0944	1	Inlet	EPA 3A, 6C	1	SO ₂
0844-0944	1	Outlet	EPA 3A, 6C, 7E, 10	1	SO ₂ , NO _x , CO
0853-0953	1	Outlet	EPA 9	1	VE
1520-1727	1	Outlet	EPA 5/26	2	PM/HCl
1520-1720	1	Inlet	EPA 26	2	HCl
1528-1628	1	Outlet	EPA 9	2	VE
1552-1727	1	Inlet	EPA 3A, 6C	2	SO ₂
1552-1652	1	Outlet	EPA 3A, 6C, 7E, 10	2	SO ₂ , NO _x , CO
1628-1728	1	Outlet	EPA 9	3	VE
1752-2000	1	Outlet	EPA 5/26	3	PM/HCl
1755-1955	1	Inlet	EPA 26	3	HCl
1756-1856	1	Inlet	EPA 3A, 6C	3	SO ₂
1756-1856	1	Outlet	EPA 3A, 6C, 7E, 10	3	SO ₂ , NO _x , CO
<u>1/27/99</u>					
0840-1107	1	Inlet	EPA 29	(1) ⁽¹⁾	Hg
0840-1111	1	Outlet	EPA 29	(1)	Hg
1140-1350	1	Inlet	EPA 29	1(2)	Hg
1140-1350	1	Outlet	EPA 29	1(2)	Hg
1420-1647	1	Inlet	EPA 29	2(3)	Hg
1420-1648	1	Outlet	EPA 29	2(3)	Hg
1710-1920	1	Inlet	EPA 29	3(4)	Hg
1713-1920	1	Outlet	EPA 29	3(4)	Hg
<u>1/28/99</u>					
0827-1035	2	Inlet	EPA 29	1	Hg
0827-1035	2	Outlet	EPA 29	1	Hg
1340-1546	2	Inlet	EPA 29	2	Hg
1340-1548	2	Outlet	EPA 29	2	Hg
1615-1822	2	Inlet	EPA 29	3	Hg
1615-1822	2	Outlet	EPA 29	3	Hg
<u>1/29/99</u>					
0800-1000	2	Inlet	EPA 26	1	HCl
0800-1005	2	Outlet	EPA 5/26	1	PM/HCl
0806-0906	2	Outlet	EPA 9	1	VE
0840-0940	2	Inlet	EPA 3A, 6C	1	SO ₂
0840-0940	2	Stack	EPA 3A, 6C, 7E, 10	1	SO ₂ , NO _x , CO
1028-1235	2	Outlet	EPA 5/26	2	PM/HCl
1032-1132	2	Inlet	EPA 3A, 6C	2	SO ₂
1032-1132	2	Outlet	EPA 3A, 6C, 7E, 10	2	SO ₂ , NO _x , CO
1032-1242	2	Inlet	EPA 26	2	HCl
1033-1133	2	Outlet	EPA 9	2	VE
1300-1553	2	Inlet	EPA 26	3	HCl
1300-1551	2	Outlet	EPA 5/26	3	PM/HCl
1307-1407	2	Inlet	EPA 3A, 6C	3	SO ₂
1307-1407	2	Outlet	EPA 3A, 6C, 7E, 10	3	SO ₂ , NO _x , CO
1313-1413	2	Outlet	EPA 9	3	VE

⁽¹⁾ First mercury test runs for unit one were voided due to the lower quantities of medical waste being processed.

4.0 OPERATIONAL DATA DURING EMISSION TESTING

4.0 OPERATIONAL DATA DURING EMISSION TESTING

Operational data were collected from process recorders. This confidential data is shown in Volume 3.

5.0 METHODOLOGY

TABLE 5.1
REFERENCES

Parameter	Test Method	Reference
PM	U.S. EPA Method 5	40 CFR 60, App. A
SO ₂	U.S. EPA Method 6C	40 CFR 60, App. A
NO _x	U.S. EPA Method 7E	40 CFR 60, App. A
CO	U.S. EPA Method 10	40 CFR 60, App. A
VE	U.S. EPA Method 9	40 CFR 60, App. A
HCl	U.S. EPA Method 26	40 CFR 60, App. A
Hg	U.S. EPA Method 29	40 CFR 60, App. A

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Florida Medical route pickup

4/26/99

SITE	TRUCK NUM	TRUCK CODE	HAUL NAME	REFUS NAME	TONS	IN DATE	IN TIME	DEPT
1	64065	237	Town & Country Ref	GARBAGE	13.99	4/7/99	08:12:03	WED
1	64104	237	Town & Country Ref	GARBAGE	11.55	4/7/99	11:53:50	WED
1	64135	237	Town & Country Ref	GARBAGE	9.53	4/7/99	14:55:27	WED
1	64769	237	Town & Country Ref	GARBAGE	12.97	4/14/99	08:12:33	WED
1	64814	237	Town & Country Ref	GARBAGE	12.5	4/14/99	12:07:48	WED
1	64857	237	Town & Country Ref	GARBAGE	9.45	4/14/99	15:02:39	WED
2	1048447	235	Town & Country Ref	GARBAGE	10.92	11/4/98	08:58:39	WED
2	1048465	235	Town & Country Ref	GARBAGE	6.78	11/4/98	11:23:30	WED
2	1048906	235	Town & Country Ref	GARBAGE	12.38	11/11/98	08:29:42	WED
2	1048920	235	Town & Country Ref	GARBAGE	5.53	11/11/98	10:19:30	WED
2	1048943	235	Town & Country Ref	GARBAGE	10.93	11/11/98	13:44:10	WED
2	1049370	235	Town & Country Ref	GARBAGE	13.43	11/18/98	08:14:53	WED
2	1049384	235	Town & Country Ref	GARBAGE	8.11	11/18/98	10:22:18	WED
2	1049404	235	Town & Country Ref	GARBAGE	11.56	11/18/98	13:44:24	WED
2	1049833	235	Town & Country Ref	GARBAGE	12.86	11/25/98	07:44:52	WED
2	1049851	235	Town & Country Ref	GARBAGE	12.17	11/25/98	10:23:27	WED
2	1050264	235	Town & Country Ref	GARBAGE	11.03	12/2/98	08:23:04	WED
2	1050281	235	Town & Country Ref	GARBAGE	4.67	12/2/98	10:29:55	WED
2	1050317	235	Town & Country Ref	GARBAGE	9.66	12/2/98	14:42:09	WED
2	1050783	235	Town & Country Ref	GARBAGE	12.49	12/9/98	08:23:45	WED
2	1050793	235	Town & Country Ref	GARBAGE	5.34	12/9/98	10:06:12	WED
2	1050814	235	Town & Country Ref	GARBAGE	11.43	12/9/98	13:05:26	WED
2	1051268	235	Town & Country Ref	GARBAGE	15.94	12/16/98	08:26:55	WED
2	1051278	235	Town & Country Ref	GARBAGE	6.03	12/16/98	10:14:45	WED
2	1051303	235	Town & Country Ref	GARBAGE	10.75	12/16/98	13:46:07	WED
2	1051749	235	Town & Country Ref	GARBAGE	11.86	12/23/98	08:06:54	WED
2	1051773	235	Town & Country Ref	GARBAGE	10.01	12/23/98	11:15:24	WED
2	1051804	235	Town & Country Ref	GARBAGE	11.94	12/23/98	15:08:17	WED
2	1052202	235	Town & Country Ref	GARBAGE	10.97	12/30/98	08:12:35	WED
2	1052221	235	Town & Country Ref	GARBAGE	12.8	12/30/98	10:59:50	WED
2	1052250	235	Town & Country Ref	GARBAGE	7	12/30/98	13:58:19	WED
2	1052681	235	Town & Country Ref	GARBAGE	12.36	1/6/99	08:30:49	WED
2	1052709	235	Town & Country Ref	GARBAGE	5.69	1/6/99	12:08:00	WED

10

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Florida Medical route pickup

4/26/99

SITE	TICKNON	TRUCK CODE	HALL NAME	REFUSAL	TONS	IN DATE	IN TIME	DOWN
2	1052735	235	Town & Country Ref	GARBAGE	13.38	1/6/99	15:53:00	WED
2	1053205	235	Town & Country Ref	GARBAGE	14.14	1/13/99	08:24:19	WED
2	1053219	235	Town & Country Ref	GARBAGE	6.82	1/13/99	10:24:02	WED
2	1053713	235	Town & Country Ref	GARBAGE	7.42	1/20/99	10:09:57	WED
2	1053750	235	Town & Country Ref	GARBAGE	12.58	1/20/99	13:59:21	WED
2	1054223	235	Town & Country Ref	GARBAGE	15.32	1/27/99	09:15:16	WED
2	1054242	235	Town & Country Ref	GARBAGE	10.78	1/27/99	11:51:51	WED
2	1054282	235	Town & Country Ref	GARBAGE	12.67	1/27/99	16:27:15	WED
2	1054725	235	Town & Country Ref	GARBAGE	14.37	2/3/99	08:01:48	WED
2	1054738	235	Town & Country Ref	GARBAGE	8.57	2/3/99	10:13:51	WED
2	1054756	235	Town & Country Ref	GARBAGE	8.45	2/3/99	12:28:26	WED
2	1054779	235	Town & Country Ref	GARBAGE	6.3	2/3/99	14:44:46	WED
2	1055251	235	Town & Country Ref	GARBAGE	13.76	2/10/99	08:14:19	WED
2	1055261	235	Town & Country Ref	GARBAGE	6.9	2/10/99	10:05:28	WED
2	1055283	235	Town & Country Ref	GARBAGE	11.78	2/10/99	12:52:24	WED
2	1055305	235	Town & Country Ref	GARBAGE	5.96	2/10/99	15:08:41	WED
2	1055785	235	Town & Country Ref	GARBAGE	13.59	2/17/99	08:34:32	WED
2	1055794	235	Town & Country Ref	GARBAGE	7.78	2/17/99	10:43:08	WED
2	1055821	235	Town & Country Ref	GARBAGE	11.99	2/17/99	14:03:23	WED
2	1055846	235	Town & Country Ref	GARBAGE	8.93	2/17/99	16:34:56	WED
2	1056311	235	Town & Country Ref	GARBAGE	12.59	2/24/99	07:56:43	WED
2	1056333	235	Town & Country Ref	GARBAGE	11.13	2/24/99	10:12:05	WED
2	1056348	235	Town & Country Ref	GARBAGE	6.95	2/24/99	12:03:19	WED
2	1056384	235	Town & Country Ref	GARBAGE	11.82	2/24/99	15:10:04	WED
2	1056403	235	Town & Country Ref	GARBAGE	6.19	2/24/99	17:03:14	WED
2	1056884	235	Town & Country Ref	GARBAGE	11.11	3/3/99	08:02:48	WED
2	1056904	235	Town & Country Ref	GARBAGE	10.42	3/3/99	10:40:59	WED
2	1056927	235	Town & Country Ref	GARBAGE	11.5	3/3/99	13:26:35	WED
2	1056957	235	Town & Country Ref	GARBAGE	10.91	3/3/99	16:32:32	WED
2	1057452	235	Town & Country Ref	GARBAGE	14.01	3/10/99	08:16:22	WED
2	1057490	235	Town & Country Ref	GARBAGE	8.09	3/10/99	13:14:32	WED
2	1057521	235	Town & Country Ref	GARBAGE	12.47	3/10/99	16:44:39	WED
2	1058565	237	TOWN & COUNTRY	GARBAGE	12.59	3/24/99	08:15:46	WED

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Florida Medical route pickup

4/26/99

SITE	TIC #	TRUCK #	TOWN	TYPE	TIME	DATE	TIME	DAY
2	1058582	237	TOWN & COUNTRY	GARBAGE	7.67	3/24/99	10:22:27	WED
2	1058615	237	TOWN & COUNTRY	GARBAGE	12.1	3/24/99	13:59:26	WED
2	1058643	237	TOWN & COUNTRY	GARBAGE	9.5	3/24/99	16:36:08	WED
2	1059140	237	TOWN & COUNTRY	GARBAGE	11.97	3/31/99	08:24:04	WED
2	1059158	237	TOWN & COUNTRY	GARBAGE	6.18	3/31/99	10:26:38	WED
2	1059181	237	TOWN & COUNTRY	GARBAGE	8.65	3/31/99	12:41:34	WED
2	1059214	237	TOWN & COUNTRY	GARBAGE	9.97	3/31/99	16:08:33	WED
2	1060112	237	TOWN & COUNTRY	GARBAGE	13.08	4/21/99	08:37:02	WED
2	1060144	237	TOWN & COUNTRY	GARBAGE	12.21	4/21/99	12:31:04	WED
2	1060170	237	TOWN & COUNTRY	GARBAGE	9.47	4/21/99	14:51:51	WED
2	1060206	237	TOWN & COUNTRY	GARBAGE	11.99	4/22/99	08:32:19	THU



Interim Remedial Action Plan

**Florida Medical Industries, Inc.
Leesburg, Lake County, Florida**

Prepared for:

Florida Medical Industries, Inc.
P.O. Box 493000
Leesburg, Florida 34749-3000

Prepared by:

Kraus GeoEnvironmental Services, Inc.
P.O. Box 1745
Safety Harbor, Florida 34695-1745

October 1995

runoff away from the excavations and stockpiles, and to minimize sediment erosion and runoff from the excavation sites.

At each glass area, soil will be stockpiled on an impervious surface consisting of several layers of plastic sheeting. The stockpile will be similarly covered with plastic sheeting.

If necessary, partial or completely encircling berms will be placed around the excavations and stockpiles to divert surface water runoff from entering these areas. The necessity of installing diversion berms will depend on ground surface slope and runoff potential, and will be assessed at each glass area.

Excessive erosion is not expected to occur in most of the glass areas, but, if necessary, filter fences will be installed downslope from excavation area(s) to prevent offsite transport of sediment.

3.5 Treatment Methodology

As discussed previously, treatment of the glass fragments will be conducted using FMI's retort for mercury recovery. The retort system consists of a vertical vacuum chamber manufactured by T-M Vacuum Products, Inc. and measures 30 inches by 48 inches in depth. The system also contains a Leybold Model D30A vacuum system, a mechanically refrigerated cold trap system consisting of a compressor refrigeration package with a hot gas defrost unit and a stainless trap.

In the treatment process, scrap thermometers are loaded into a specially constructed stainless steel 55-gallon vessel which is placed in the vacuum chamber and heated to approximately 1100°F for 22 hours. The generated vapors are drawn through the chilled condenser unit where they liquify and are collected after a 24 hour cooling period. The recovered mercury is collected in metal flasks with a capacity of 70 pounds, and are collected by a vendor for triple distillation and reuse. The remaining scrap glass is first visually inspected for visible mercury, a test sample is collected for mercury TCLP analysis, and the glass is tagged and stored pending receipt of the analytical test results.

Monthly analytical tests conducted by FMI have shown that the majority of the analyses indicated that mercury TCLP concentrations were below the method detection limit. Mercury is occasionally detected in the post-treatment glass samples, but at concentrations below the TCLP threshold of 200 ug/l. The treated glass fragments are removed from the site by Town and Country (waste hauler) and transported to the Lake County incinerator for final disposal.

The capacity of the retort per load is approximately 55 gallons. The facility is permitted to operate 16 hours/day, 5 days/week, 52 weeks/year. The system capacity is approximately 10-12 loads per month, with current manufacturing operations producing approximately 4 loads/month. Given the permitted capacity and allowing for existing plant production

requirements, approximately 6 loads per month capacity is available for treatment of the glass fragments recovered in the IRA. The available capacity of the system, coupled with the limitations regarding the duration of storage of the pre-treated glass, constitute the schedule-limiting factor for the IRA. The resultant schedule for the IRA is discussed in Section 5.

3.6 Disposition of Post-treatment Materials

This section addresses the plan for disposal of the treated glass fragments and stockpiled soil discussed in previous sections of this plan.

Testing conducted by FMI has demonstrated that the treated glass fragments from the retort are non-hazardous in nature, and can be disposed through FMI's existing contracted waste hauler Town and Country.

During the IRA, samples of the stockpiled (post-separation) soil will be analyzed for total mercury and TCLP mercury. Soil action levels will follow the cleanup goals described in FDEP's August 25, 1995 memorandum from Ligia Mora-Applegate to FDEP Waste Program Administrators and the attachment to the memorandum entitled "Updated Soil Cleanup Goals, Based on Direct Exposure and Migration to Groundwater, August 18, 1995." This document lists action levels for soil 0-2 ft bls for mercury under residential land use (23 mg/kg) and industrial land use (480 mg/kg). The document further states that if the industrial land use scenario is employed, the site must have a deed restriction for the more restrictive land use. A leachability-based goal for soils below 2 ft bls is discussed for certain compounds in the memorandum, but a leachability-based goal was not reported for mercury. Subsequent discussions with FDEP District staff confirmed that a leachability-based goal is not available (telephone conversation of September 27, 1995, George Houston and Bret Leroux, FDEP Central District office with David Kraus, KGS). FDEP staff suggested the following cleanup goals for soils greater than 2 ft bls: in areas where mercury concentrations exceed the state maximum contaminant level of 2 micrograms per liter (2 ug/l), the TCLP criterion of 200 ug/l can be used; in other areas, the residential or industrial land use soil cleanup goal of 23 mg/kg or 480 mg/kg, respectively. It is FMI's intention at this time to employ the more conservative residential land use soil cleanup goal of 23 mg/kg as the IRA action level for both the 0-2 ft bls soils and for soils below 2 ft bls, unless site conditions warrant selection of the industrial land use goal of 480 mg/kg.

For soil stockpiles containing total mercury concentrations below the action level, FMI will backfill the stockpiled soil at each glass area into the original excavation.

Soil stockpiles with total mercury concentrations above the action level will be removed from the site by a licensed waste disposal firm and transported to a permitted facility for pretreatment (if necessary) and final disposal.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 26, 1998

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: 1346.0 KLB	STEAM PRODUCED: 1407.0 KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: 1356.0 KLB	FEEDWATER USED: 1445.0 KLB	ENDING: 4402.0 WH TOT	BEGINNING: 162597 CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: 4392.0 WH TOT	ENDING: 162597 CU FT
BLOWDOWN: 10 KLB	BLOWDOWN: 38 KLB	TOTAL: 288.0 MWH	TOTAL USED: 0 CU FT
BLOWDOWN: 0.7 %	BLOWDOWN: 2.6 %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: 10000710 JEM TOT	ENDING: 8.8 FT/IN OUT
ENDING: 63564.3 HRS	ENDING: 62524.4 HRS	BEGINNING: 9762170 JEM TOT	BEGINNING: 8.3 FT/IN OUT
BEGINNING: 63540.2 HRS	BEGINNING: 62500.4 HRS	TOTAL: 238.5 MWH	RECEIVED: 0.00 TONS
TOTAL: 24.1 HRS	TOTAL: 24.0 HRS	UTILITY IN:	EOM OUT: 8.67
BOILER RUN TIME: 24.0 HRS	BOILER RUN TIME: 24.0 HRS	ENDING: 2568860 JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: 56.1 KLB/HR	AVG. STEAM FLOW: 58.6 KLB/HR	BEGINNING: 2568860 JEM TOT	USAGE UNIT #1: 288.8 LBS
APPROX REF PROC: 211.0 TONS	APPROX REF PROC: 213.0 TONS	TOTAL: 0.0 MWH	USAGE UNIT #2: 268.8 LBS
REFUSE PROCESSED: 224.3 TONS	REFUSE PROCESSED: 234.5 TONS	GENERATOR RUN TIME: 24.0 HRS	DAILY TOTAL: 537.6 LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: 49.5 MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: 2753.0 KLB	GROSS REFUSE REC: 596.57 TONS ✓	GEN RUN TIME: 24.0 HRS	ENDING: 8 FT. OUT 92 IN OUT
TOTAL REFUSE PR: 424.0 TONS	NON PROCESSED: 0.00 TONS	IN PLANT USE: 49.5 MWH	BEGINNING: 9 FT. OUT 20 IN OUT
	FERROUS HAULED: 0.00 TONS ✓	KWH/TON: 116.7	RECEIVED: 0.00 TONS
	TOTAL REFUSE REC: 596.57 TONS ✓		EOM OUT: 15.67
WELL WATER USE:	EST PIT INVENTORY: 2,859.0 TONS	MEDICAL WASTE:	
ENDING: 286695000 GAL	ASH HAULED: 0.00 TONS	PROCESSED: 0.00 TONS	
BEGINNING: 286382000 GAL		% OF REFUSE PROC: 0.00 %	
TOTAL USED: 313000 GAL	208.16		
UNIT 1 AVAILABILITY: 100.0 %	UNIT 2 AVAILABILITY: 100.0 %	TG AVAILABILITY: 100.0 %	
UNIT 1 % MCR: 87.1 %	UNIT 2 % MCR: 91.0 %	TG % MCR: 76.4 %	
LB STEAM/LB PR: 3.0	LB STEAM/GROSS KW: 9.6	GROSS KW/TON PR: 679.2	
NET KWH/TON PR: 562.5	LB LIME/TON PR: 3.7	TOT STM TO T/G: 2.776.0	

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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 27, 1998

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1452.0</u> KLB	STEAM PRODUCED: <u>1500.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1479.0</u> KLB	FEEDWATER USED: <u>1588.0</u> KLB	ENDING: <u>4413.0</u> WH TOT	BEGINNING: <u>162597</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>4402.0</u> WH TOT	ENDING: <u>162598</u> CU FT
BLOWDOWN: <u>27</u> KLB	BLOWDOWN: <u>88</u> KLB	TOTAL: <u>316.8</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>1.8</u> %	BLOWDOWN: <u>5.5</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>266050</u> JEM TOT	ENDING: <u>4.0</u> FT/IN OUT
ENDING: <u>63588.2</u> HRS	ENDING: <u>62548.4</u> HRS	BEGINNING: <u>710</u> JEM TOT	BEGINNING: <u>8.8</u> FT/IN OUT
BEGINNING: <u>63564.3</u> HRS	BEGINNING: <u>62524.4</u> HRS	TOTAL: <u>265.3</u> MWH	RECEIVED: <u>26.29</u> TONS
TOTAL: <u>23.9</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>4.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2568880</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>60.5</u> KLB/HR	AVG. STEAM FLOW: <u>62.5</u> KLB/HR	BEGINNING: <u>2568880</u> JEM TOT	USAGE UNIT #1: <u>268.8</u> LBS
APPROX REF PROC: <u>222.0</u> TONS	APPROX REF PROC: <u>263.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>268.8</u> LBS
REFUSE PROCESSED: <u>242.0</u> TONS	REFUSE PROCESSED: <u>250.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>537.6</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>51.5</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>102.1</u>	ENDING: <u>9</u> FT. OUT <u>0</u> IN OUT
TOTAL STEAM FLOW: <u>2952.0</u> KLB	GROSS REFUSE REC: <u>581.24</u> TONS ✓		BEGINNING: <u>8</u> FT. OUT <u>92</u> IN OUT
TOTAL REFUSE PR. <u>504.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>17.37</u> TONS ✓		EOM OUT: <u>9.00</u>
	TOTAL REFUSE REC: <u>563.87</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>2,976.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>287031000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>19.00</u> TONS	
BEGINNING: <u>286695000</u> GAL		% OF REFUSE PROC: <u>3.77</u> %	
TOTAL USED: <u>336000</u> GAL	<u>202.88</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>93.9</u> %	UNIT 2 % MCR: <u>97.0</u> %	TG % MCR: <u>84.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.3</u>	GROSS KW/TON PR. <u>628.6</u>	
NET KWH/TON PR. <u>526.5</u>	LB LIME/TON PR.: <u>74.4</u>	TOT STM TO T/G: <u>3,036.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 28, 1998

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1295.3</u> KLB	STEAM PRODUCED: <u>1497.2</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1308.4</u> KLB	FEEDWATER USED: <u>1584.8</u> KLB	ENDING: <u>4423.0</u> WH TOT	BEGINNING: <u>162598</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>4413.0</u> WH TOT	ENDING: <u>162599</u> CU FT
BLOWDOWN: <u>13.1</u> KLB	BLOWDOWN: <u>87.6</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN %: <u>1.0</u> %	BLOWDOWN %: <u>5.5</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>509590</u> JEM TOT	ENDING: <u>4.6</u> FT/IN OUT
ENDING: <u>63612.2</u> HRS	ENDING: <u>62572.4</u> HRS	BEGINNING: <u>266050</u> JEM TOT	BEGINNING: <u>4.0</u> FT/IN OUT
BEGINNING: <u>63588.2</u> HRS	BEGINNING: <u>62548.4</u> HRS	TOTAL: <u>243.5</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>4.50</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2568880</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>54.0</u> KLB/HR	AVG. STEAM FLOW: <u>62.4</u> KLB/HR	BEGINNING: <u>2568880</u> JEM TOT	USAGE UNIT #1: <u>268.8</u> LBS
APPROX REF PROC: <u>200.0</u> TONS	APPROX REF PROC: <u>251.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>268.8</u> LBS
REFUSE PROCESSED: <u>215.9</u> TONS	REFUSE PROCESSED: <u>249.5</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>537.6</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>44.5</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2792.5</u> KLB	GROSS REFUSE REC: <u>563.79</u> TONS ✓	KWH/TON: <u>86.1</u>	ENDING: <u>8</u> FT. OUT <u>9</u> IN OUT
TOTAL REFUSE PR. <u>462.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>9</u> FT. OUT <u>0</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>22.50</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
ENDING: <u>287338000</u> GAL	TOTAL REFUSE REC: <u>541.29</u> TONS ✓	MEDICAL WASTE :	EOM OUT: <u>8.75</u>
BEGINNING: <u>287031000</u> GAL	EST PIT INVENTORY: <u>3,151.0</u> TONS	PROCESSED: <u>11.69</u> TONS	
TOTAL USED: <u>307000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.53</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>83.8</u> %	UNIT 2 % MCR: <u>96.9</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.7</u>	GROSS KW/TON PR. <u>622.4</u>	
NET KWH/TON PR. <u>526.4</u>	LB LIME/TON PR.: <u>4.1</u>	TOT STM TO T/G: <u>2,814.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 29, 1998

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1414.0</u> KLB	STEAM PRODUCED: <u>1487.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1428.0</u> KLB	FEEDWATER USED: <u>1575.0</u> KLB	ENDING: <u>4433.0</u> WH TOT	BEGINNING: <u>162599</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>4423.0</u> WH TOT	ENDING: <u>162603</u> CU FT
BLOWDOWN: <u>14</u> KLB	BLOWDOWN: <u>88</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>4</u> CU FT
BLOWDOWN: <u>1.0</u> %	BLOWDOWN: <u>5.6</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>764640</u> JEM TOT	ENDING: <u>5.2</u> FT/IN OUT
ENDING: <u>63636.1</u> HRS	ENDING: <u>62596.3</u> HRS	BEGINNING: <u>509590</u> JEM TOT	BEGINNING: <u>4.6</u> FT/IN OUT
BEGINNING: <u>63612.2</u> HRS	BEGINNING: <u>62572.4</u> HRS	TOTAL: <u>255.1</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>23.9</u> HRS	TOTAL: <u>23.9</u> HRS	UTILITY IN:	EOM OUT: <u>5.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2568880</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>58.9</u> KLB/HR	AVG. STEAM FLOW: <u>62.0</u> KLB/HR	BEGINNING: <u>2568880</u> JEM TOT	USAGE UNIT #1: <u>268.8</u> LBS
APPROX REF PROC: <u>181.0</u> TONS	APPROX REF PROC: <u>229.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>268.8</u> LBS
REFUSE PROCESSED: <u>235.7</u> TONS	REFUSE PROCESSED: <u>247.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>537.0</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>33.0</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2901.0</u> KLB	GROSS REFUSE REC: <u>477.75</u> TONS ✓	KWH/TON: <u>76.9</u>	ENDING: <u>8</u> FT. OUT <u>7</u> IN OUT
TOTAL REFUSE PR. <u>428.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>8</u> FT. OUT <u>9</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
ENDING: <u>287634000</u> GAL	TOTAL REFUSE REC: <u>477.75</u> TONS ✓	MEDICAL WASTE :	EOM OUT: <u>8.58</u>
BEGINNING: <u>287338000</u> GAL	EST PIT INVENTORY: <u>2,567.5</u> TONS	PROCESSED: <u>18.54</u> TONS	
TOTAL USED: <u>296000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>4.33</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>91.5</u> %	UNIT 2 % MCR: <u>96.2</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.1</u>	GROSS KW/TON PR. <u>672.0</u>	
NET KWH/TON PR. <u>595.2</u>	LB LIME/TON PR.: <u>4.4</u>	TOT STM TO T/G: <u>2,940.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 25, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1283.0</u> KLB	STEAM PRODUCED: <u>1261.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1511.0</u> KLB	FEEDWATER USED: <u>1297.0</u> KLB	ENDING: <u>7647.0</u> WH TOT	BEGINNING: <u>173489</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7638.0</u> WH TOT	ENDING: <u>173491</u> CU FT
BLOWDOWN: <u>228</u> KLB	BLOWDOWN: <u>36</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>2</u> CU FT
BLOWDOWN %: <u>15.1</u> %	BLOWDOWN %: <u>2.8</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>7477210</u> JEM TOT	ENDING: <u>9.0</u> FT/IN OUT
ENDING: <u>72248.9</u> HRS	ENDING: <u>71218.4</u> HRS	BEGINNING: <u>7268100</u> JEM TOT	BEGINNING: <u>8.9</u> FT/IN OUT
BEGINNING: <u>72224.9</u> HRS	BEGINNING: <u>71194.4</u> HRS	TOTAL: <u>209.1</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>53.5</u> KLB/HR	AVG. STEAM FLOW: <u>52.5</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>251.8</u> TONS	APPROX REF PROC: <u>216.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>213.8</u> TONS	REFUSE PROCESSED: <u>210.2</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>50.1</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2544.0</u> KLB	GROSS REFUSE REC: <u>683.03</u> TONS	KWH/TON: <u>118.1</u>	ENDING: <u>14</u> FT. OUT <u>80</u> IN OUT
TOTAL REFUSE PR. <u>424.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>14</u> FT. OUT <u>95</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
ENDING: <u>391829000</u> GAL	TOTAL REFUSE REC: <u>683.03</u> TONS ✓	MEDICAL WASTE:	EOM OUT: <u>20.67</u>
BEGINNING: <u>391558000</u> GAL	EST PIT INVENTORY: <u>1,867.0</u> TONS	PROCESSED: <u>0.00</u> TONS	
TOTAL USED: <u>271000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.00</u> %	
	<u>126.79</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>83.0</u> %	UNIT 2 % MCR: <u>81.6</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.8</u>	GROSS KW/TON PR. <u>611.3</u>	
NET KWH/TON PR. <u>493.2</u>	LB LIME/TON PR.: <u>0.7</u>	TOT STM TO T/G: <u>2,538.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

13

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 26, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1388.0</u> KLB	STEAM PRODUCED: <u>1263.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1634.5</u> KLB	FEEDWATER USED: <u>1295.5</u> KLB	ENDING: <u>7658.0</u> WH TOT	BEGINNING: <u>173491</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7647.0</u> WH TOT	ENDING: <u>173497</u> CU FT
BLOWDOWN: <u>247</u> KLB	BLOWDOWN: <u>33</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>6</u> CU FT
BLOWDOWN %: <u>15.1</u> %	BLOWDOWN %: <u>2.5</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>7693000</u> JEM TOT	ENDING: <u>9.9</u> FT/IN OUT
ENDING: <u>72272.9</u> HRS	ENDING: <u>71242.4</u> HRS	BEGINNING: <u>7477210</u> JEM TOT	BEGINNING: <u>9.0</u> FT/IN OUT
BEGINNING: <u>72248.9</u> HRS	BEGINNING: <u>71218.4</u> HRS	TOTAL: <u>215.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.75</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>57.8</u> KLB/HR	AVG. STEAM FLOW: <u>52.8</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>231.3</u> TONS	APPROX REF PROC: <u>210.5</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>231.3</u> TONS	REFUSE PROCESSED: <u>210.5</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>43.4</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>94.8</u>	ENDING: <u>14</u> FT. OUT <u>54</u> IN OUT
TOTAL STEAM FLOW: <u>2651.0</u> KLB	GROSS REFUSE REC: <u>691.81</u> TONS		BEGINNING: <u>14</u> FT. OUT <u>80</u> IN OUT
TOTAL REFUSE PR. <u>458.1</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>18.50</u>
ENDING: <u>392108000</u> GAL	TOTAL REFUSE REC: <u>691.81</u> TONS ✓	MEDICAL WASTE:	
BEGINNING: <u>391829000</u> GAL	EST PIT INVENTORY: <u>2,217.0</u> TONS	PROCESSED: <u>16.27</u> TONS	
TOTAL USED: <u>279000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>3.55</u> %	
	<u>97.60</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>89.8</u> %	UNIT 2 % MCR: <u>81.7</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>565.9</u>	
NET KWH/TON PR. <u>471.1</u>	LB LIME/TON PR.: <u>6.2</u>	TOT STM TO T/G: <u>2,831.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 27, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1374.7</u> KLB	STEAM PRODUCED: <u>1263.2</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1610.6</u> KLB	FEEDWATER USED: <u>1297.2</u> KLB	ENDING: <u>7665.0</u> WH TOT	BEGINNING: <u>173497</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7656.0</u> WH TOT	ENDING: <u>173497</u> CU FT
BLOWDOWN: <u>236</u> KLB	BLOWDOWN: <u>34</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>14.6</u> %	BLOWDOWN: <u>2.6</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>7902030</u> JEM TOT	ENDING: <u>7.0</u> FT/IN OUT
ENDING: <u>72296.9</u> HRS	ENDING: <u>71268.4</u> HRS	BEGINNING: <u>7693000</u> JEM TOT	BEGINNING: <u>9.9</u> FT/IN OUT
BEGINNING: <u>72272.9</u> HRS	BEGINNING: <u>71242.4</u> HRS	TOTAL: <u>209.0</u> MWH	RECEIVED: <u>24.75</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>7.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>57.3</u> KLB/HR	AVG. STEAM FLOW: <u>52.6</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>228.0</u> TONS	APPROX REF PROC: <u>177.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>229.1</u> TONS	REFUSE PROCESSED: <u>210.5</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>50.2</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>119.0</u>	ENDING: <u>14</u> FT. OUT <u>32</u> IN OUT
TOTAL STEAM FLOW: <u>2637.9</u> KLB	GROSS REFUSE REC: <u>621.37</u> TONS		BEGINNING: <u>14</u> FT. OUT <u>54</u> IN OUT
TOTAL REFUSE PR. <u>421.6</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS		EOM OUT: <u>16.87</u>
	TOTAL REFUSE REC: <u>621.37</u> TONS		
WELL WATER USE:	EST PIT INVENTORY: <u>2,450.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>392384000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>16.60</u> TONS	
BEGINNING: <u>392108000</u> GAL		% OF REFUSE PROC: <u>3.94</u> %	
TOTAL USED: <u>276000</u> GAL	<u>144.08</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>88.9</u> %	UNIT 2 % MCR: <u>61.7</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>614.8</u>	
NET KWH/TON PR. <u>495.8</u>	LB LIME/TON PR.: <u>95.8</u>	TOT STM TO T/G: <u>2,590.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 28, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1321.4</u> KLB	STEAM PRODUCED: <u>1464.3</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1546.7</u> KLB	FEEDWATER USED: <u>1495.1</u> KLB	ENDING: <u>7674.0</u> WH TOT	BEGINNING: <u>173497</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7685.0</u> WH TOT	ENDING: <u>173497</u> CU FT
BLOWDOWN: <u>225</u> KLB	BLOWDOWN: <u>31</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN %: <u>14.6</u> %	BLOWDOWN %: <u>2.1</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>8130990</u> JEM TOT	ENDING: <u>7.5</u> FT/IN OUT
ENDING: <u>72320.9</u> HRS	ENDING: <u>71290.4</u> HRS	BEGINNING: <u>7902030</u> JEM TOT	BEGINNING: <u>7.0</u> FT/IN OUT
BEGINNING: <u>72296.9</u> HRS	BEGINNING: <u>71266.4</u> HRS	TOTAL: <u>229.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>7.42</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.1</u> KLB/HR	AVG. STEAM FLOW: <u>61.0</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>215.0</u> TONS	APPROX REF PROC: <u>208.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>220.2</u> TONS	REFUSE PROCESSED: <u>244.1</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>30.2</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>71.5</u>	ENDING: <u>14</u> FT. OUT <u>28</u> IN OUT
TOTAL STEAM FLOW: <u>2785.7</u> KLB	GROSS REFUSE REC: <u>533.27</u> TONS		BEGINNING: <u>14</u> FT. OUT <u>32</u> IN OUT
TOTAL REFUSE PR. <u>423.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>16.33</u>
ENDING: <u>392679000</u> GAL	TOTAL REFUSE REC: <u>533.27</u> TONS ✓	MEDICAL WASTE:	
BEGINNING: <u>392384000</u> GAL	EST PIT INVENTORY: <u>2,509.0</u> TONS	PROCESSED: <u>0.00</u> TONS	
TOTAL USED: <u>285000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.00</u> %	
	<u>142.98</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.5</u> %	UNIT 2 % MCR: <u>94.7</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.7</u>	GROSS KW/TON PR. <u>612.8</u>	
NET KWH/TON PR. <u>541.3</u>	LB LIME/TON PR.: <u>3.7</u>	TOT STM TO T/G: <u>2,775.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 29, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1366.0</u> KLB	STEAM PRODUCED: <u>1505.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1593.1</u> KLB	FEEDWATER USED: <u>1534.1</u> KLB	ENDING: <u>7684.0</u> WH TOT	BEGINNING: <u>173497</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7674.0</u> WH TOT	ENDING: <u>173497</u> CU FT
BLOWDOWN: <u>227</u> KLB	BLOWDOWN: <u>29</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN %: <u>14.3</u> %	BLOWDOWN %: <u>1.9</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>8369940</u> JEM TOT	ENDING: <u>8.0</u> FT/IN OUT
ENDING: <u>72344.9</u> HRS	ENDING: <u>71314.4</u> HRS	BEGINNING: <u>8130990</u> JEM TOT	BEGINNING: <u>7.5</u> FT/IN OUT
BEGINNING: <u>72320.9</u> HRS	BEGINNING: <u>71290.4</u> HRS	TOTAL: <u>239.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>8.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>56.9</u> KLB/HR	AVG. STEAM FLOW: <u>62.7</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>210.0</u> TONS	APPROX REF PROC: <u>231.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>227.7</u> TONS	REFUSE PROCESSED: <u>250.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>49.1</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2871.0</u> KLB	GROSS REFUSE REC: <u>592.34</u> TONS	KWH/TON: <u>109.7</u>	ENDING: <u>14</u> FT. OUT <u>23</u> IN OUT
TOTAL REFUSE PR. <u>447.1</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>14</u> FT. OUT <u>28</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>18.73</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
ENDING: <u>392985000</u> GAL	TOTAL REFUSE REC: <u>573.61</u> TONS ✓	MEDICAL WASTE:	EOM OUT: <u>15.92</u>
BEGINNING: <u>392679000</u> GAL	EST PIT INVENTORY: <u>2,392.0</u> TONS	PROCESSED: <u>6.05</u> TONS	
TOTAL USED: <u>306000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.35</u> %	
	<u>109.09</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>88.4</u> %	UNIT 2 % MCR: <u>97.4</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.0</u>	GROSS KW/TON PR. <u>644.2</u>	
NET KWH/TON PR. <u>534.5</u>	LB LIME/TON PR.: <u>3.5</u>	TOT STM TO T/G: <u>2,869.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

14 ISOKINETIC SAMPLING TRAIN RESULTS - METHOD

M29

Client Name	Ogden Energy Group, Inc.	Operator	WHH, JPD
Plant Name	Lake County Resource Recovery Facility	Project #	10053
Sampling Location	Unit No. 1 SDA Inlet	Standard Temperature, °F	68

USE IN AVERAGE OF RUN SET? 1 or 0 =>		No (0)	1	1	1	SET AVERAGE
Run Number		1-I-M29-1	1-I-M29-2	1-I-M29-3	1-I-M29-4	
Run Date		01/27/99	01/27/99	01/27/99	01/27/99	
Run Start Time	hh:mm	840	1140	1420	1710	
Run Stop Time	hh:mm	1107	1350	1647	1920	

Sampling Parameters

Meter Calibration Factor	Y	0.9975	0.9975	0.9975	0.9975	
Pitot Tube Coefficient	C _p	0.84	0.84	0.84	0.84	
Stack/Duct Static Pressure	in H ₂ O	-2.60	-2.30	-2.30	-2.60	-2.40
Stack Cross-Sectional Area	ft ²	20.25	20.25	20.25	20.25	20.25
Barometric Pressure	in Hg	30.3	30.3	30.3	30.3	30.3
Actual Nozzle Diameter	in	0.218	0.218	0.218	0.218	
Carbon Dioxide Percentage	% CO ₂	8.2	8.4	9.2	8.6	8.7
Oxygen Percentage	% O ₂	11.6	11.4	10.5	11.2	11.0
Carbon Monoxide Percentage	% CO	0.0	0.0	0.0	0.0	0.0
Nitrogen Percentage	% N ₂	80.2	80.2	80.3	80.2	80.2
Total Water Volume Collected	mL	174.3	168.2	170.6	163.8	167.5
Sample Volume	ft ³	56.852	56.171	57.955	56.077	56.734
Average Meter Temperature	°F	75	85	87	86	86
Average Stack Temperature	°F	439	436	441	437	438
Average Delta H	in H ₂ O	0.77	0.73	0.75	0.72	0.73
Total Sampling Time	min	121.5	121.5	121.5	121.5	121.5

Air Flow Parameters

Volume of Water vapor @ STP	SCF	8.204	7.917	8.030	7.710	7.886
Volume Metered @ STP	DSCF	56.752	55.038	56.602	54.813	55.484
Absolute Stack/Duct Pressure	in Hg	30.1	30.1	30.1	30.1	30.1
Absolute Meter Pressure	in Hg	30.4	30.4	30.4	30.4	30.4
Calculated Stack Moisture	% H ₂ O	12.6	12.6	12.4	12.3	12.4
Reported Stack Moisture Content	% H ₂ O	12.6	12.6	12.4	12.3	12.4
Dry Mole Fraction	decimal	0.874	0.874	0.876	0.877	0.876
Avg Differential Press. (Delta P)	in H ₂ O	0.618	0.574	0.606	0.569	0.583
Dry Gas Molecular Weight	lb/lb-mole	29.78	29.80	29.89	29.82	29.84
Wet Stack Gas Molecular Weight	lb/lb-mole	28.29	28.32	28.41	28.37	28.37
Average Stack Gas Velocity	ft/sec	57.99	55.76	57.32	55.51	56.19
Percent of Isokinetic Rate	% ISO	100.3	100.7	101.1	100.7	100.8

Air Flow Rate Results

Actual Stack Flow/Minute	ACFM	70,458	67,749	69,639	67,439	68,276
Dry Standard Stack Flow/Minute	DSCFM	36,399	35,161	36,010	35,025	35,399

Concentration and Emission Rate Data Summary

Mercury	ug	9883.73	6710.60	757.20	5783.84
Concentration ug/DSCM	ug/DSCM	6341	4186	488	3672
Concentration @ ug 12% CO ₂	ug@12%	9059	5460	681	5067
Concentration ug @ 7% O ₂	ug@7%	9278	5595	699	5191
Concentration Gr @ 12% CO ₂	Gr@12%	3.96E-03	2.39E-03	2.97E-04	2.21E-03
Emission Rate, lb/hr	lb/hr	0.835	0.565	0.0640	0.49

* Note: Run 1 was voided because of Low Medical Waste Feed Rate. Run 1 was not used in average.

ISOKINETIC SAMPLING TRAIN RESULTS - METHOD

M29

Client Name	Ogden Energy Group, Inc.	Operator	DGB
Plant Name	Lake County Resource Recovery Facility	Project #	10053
Sampling Location	Unit No. 1 FF Outlet	Standard Temperature, °F	68

USE IN AVERAGE OF RUN SET? 1 or 0 =>	No (0)	1	1	1	1	SET AVERAGE
Run Number	1-O-M29-1	1-O-M29-2	1-O-M29-3	1-O-M29-4		
Run Date	01/27/99	01/27/99	01/27/99	01/27/99		
Run Start Time	hh:mm 840	1140	1420	1713		
Run Stop Time	hh:mm 1111	1350	1648	1920		

Sampling Parameters

Meter Calibration Factor	Y	0.9819	0.9819	0.9819	0.9819	
Pitot Tube Coefficient	C _p	0.84	0.84	0.84	0.84	
Stack/Duct Static Pressure	in H ₂ O	-15.70	-15.70	-15.70	-15.70	-15.70
Stack Cross-Sectional Area	ft ²	17.36	17.36	17.36	17.36	17.36
Barometric Pressure	in Hg	30.3	30.3	30.3	30.3	30.3
Actual Nozzle Diameter	in	0.218	0.218	0.218	0.218	
Carbon Dioxide Percentage	% CO ₂	7.7	7.7	8.3	7.8	7.9
Oxygen Percentage	% O ₂	12.1	12.1	11.4	12.0	11.8
Carbon Monoxide Percentage	% CO	0.0	0.0	0.0	0.0	0.0
Nitrogen Percentage	% N ₂	80.2	80.2	80.3	80.2	80.2
Total Water Volume Collected	mL	308.4	299.5	292.2	266.9	286.2
Sample Volume	ft ³	73.716	71.594	74.634	71.502	72.577
Average Meter Temperature	°F	77	83	84	85	84
Average Stack Temperature	°F	277	278	279	278	278
Average Delta H	in H ₂ O	1.20	1.11	1.23	1.10	1.15
Total Sampling Time	min	121.5	121.5	121.5	121.5	121.5

Air Flow Parameters

Volume of Water vapor @ STP	SCF	14.516	14.097	13.754	12.563	13.471
Volume Metered @ STP	DSCF	72.289	69.372	72.176	69.069	70.206
Absolute Stack/Duct Pressure	in Hg	29.1	29.1	29.1	29.1	29.1
Absolute Meter Pressure	in Hg	30.4	30.4	30.4	30.4	30.4
Calculated Stack Moisture	% H ₂ O	16.7	16.9	16.0	15.4	16.1
Reported Stack Moisture Content	% H ₂ O	16.7	16.9	16.0	15.4	16.1
Dry Mole Fraction	decimal	0.833	0.831	0.840	0.846	0.839
Avg Differential Press. (Delta P)	in H ₂ O	0.931	0.838	0.927	0.834	0.867
Dry Gas Molecular Weight	lb/lb-mole	29.72	29.72	29.78	29.73	29.74
Wet Stack Gas Molecular Weight	lb/lb-mole	27.76	27.74	27.90	27.92	27.85
Average Stack Gas Velocity	ft/sec	66.15	62.81	65.92	62.47	63.73
Percent of Isokinetic Rate	% ISO	99.6	100.9	99.1	99.3	99.8

Air Flow Rate Results

Actual Stack Flow/Minute	ACFM	68,897	65,425	68,662	65,066	66,384
Dry Standard Stack Flow/Minute	DSCFM	40,037	37,905	40,147	38,345	38,799

Concentration and Emission Rate Data Summary

Mercury	ug	8440.96	2099.86	867.36	3802.73
Concentration ug/DSCM	ug/DSCM	4297	1027	443	1922
Concentration @ ug 12% CO ₂	ug@12%	6696	1485	682	2954
Concentration ug @ 7% O ₂	ug@7%	6787	1503	693	2994
Concentration Gr @ 12% CO ₂	Gr@12%	2.93E-03	6.49E-04	2.98E-04	1.29E-03
Emission Rate, lb/hr	lb/hr	0.610	0.155	0.0637	0.276

* Note: Run 1 was voided because of Low Medical Waste Feed Rate. Run 1 was not used in average.

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ISOKINETIC SAMPLING TRAIN RESULTS - METHOD M29

Client Name	Ogden Energy Group, Inc.	Operator	WHH, JPD
Plant Name	Lake County Resource Recovery Facility	Project #	10053
Sampling Location	Unit No. 1 SDA Inlet	Standard Temperature, °F	68

USE IN AVERAGE OF RUN SET? 1 or 0 =>	0	1	1	1	SET AVERAGE
Run Number	1-I-M29-1	1-I-M29-2	1-I-M29-3	1-I-M29-4	
Run Date	01/27/99	01/27/99	01/27/99	01/27/99	
Run Start Time	hh:mm 840	1140	1420	1710	
Run Stop Time	hh:mm 1107	1350	1647	1920	

Sampling Parameters

Meter Calibration Factor	Y	0.9975	0.9975	0.9975	0.9975	
Pitot Tube Coefficient	C _p	0.84	0.84	0.84	0.84	
Stack/Duct Static Pressure	in H ₂ O	-2.60	-2.30	-2.30	-2.60	-2.40
Stack Cross-Sectional Area	ft ²	20.25	20.25	20.25	20.25	20.25
Barometric Pressure	in Hg	30.3	30.3	30.3	30.3	30.3
Actual Nozzle Diameter	in	0.218	0.218	0.218	0.218	
Carbon Dioxide Percentage	% CO ₂	8.2	8.4	9.2	8.6	8.7
Oxygen Percentage	% O ₂	11.6	11.4	10.5	11.2	11.0
Carbon Monoxide Percentage	% CO	0.0	0.0	0.0	0.0	0.0
Nitrogen Percentage	% N ₂	80.2	80.2	80.3	80.2	80.2
Total Water Volume Collected	mL	174.3	168.2	170.6	163.8	167.5
Sample Volume	ft ³	56.852	56.171	57.955	56.077	56.734
Average Meter Temperature	°F	75	85	87	86	86
Average Stack Temperature	°F	439	436	441	437	438
Average Delta H	in H ₂ O	0.77	0.73	0.75	0.72	0.73
Total Sampling Time	min	121.5	121.5	121.5	121.5	121.5

Air Flow Parameters

Volume of Water vapor @ STP	SCF	8.204	7.917	8.030	7.710	7.888
Volume Metered @ STP	DSCF	56.752	55.038	56.602	54.813	55.484
Absolute Stack/Duct Pressure	in Hg	30.1	30.1	30.1	30.1	30.1
Absolute Meter Pressure	in Hg	30.4	30.4	30.4	30.4	30.4
Calculated Stack Moisture	% H ₂ O	12.6	12.6	12.4	12.3	12.4
Reported Stack Moisture Content	% H ₂ O	12.6	12.6	12.4	12.3	12.4
Dry Mole Fraction	decimal	0.874	0.874	0.876	0.877	0.876
Avg Differential Press. (Delta P)	in H ₂ O	0.618	0.574	0.606	0.569	0.583
Dry Gas Molecular Weight	lb/lb-mole	29.78	29.80	29.89	29.82	29.84
Wet Stack Gas Molecular Weight	lb/lb-mole	28.29	28.32	28.41	28.37	28.37
Average Stack Gas Velocity	ft/sec	57.99	55.76	57.32	55.51	56.19
Percent of Isokinetic Rate	% ISO	100.3	100.7	101.1	100.7	100.8

Air Flow Rate Results

Actual Stack Flow/Minute	ACFM	70,458	67,749	69,639	67,439	68,276
Dry Standard Stack Flow/Minute	DSCFM	36,399	35,161	36,010	35,025	35,399

Concentration and Emission Rate Data Summary

Mercury	ug	54412.00	9883.73	6710.60	757.20	5783.84
Concentration ug/DSCM	ug/DSCM	33855	6341	4186	488	3672
Concentration @ ug 12% CO ₂	ug@12%	49544	9059	5460	681	5067
Concentration ug @ 7% O ₂	ug@7%	50600	9278	5595	699	5191
Concentration Gr @ 12% CO ₂	Gr@12%	2.17E-02	3.96E-03	2.39E-03	2.97E-04	2.21E-03
Emission Rate, lb/hr	lb/hr	4.62	0.835	0.565	0.0640	0.49

* Note: Run 1 was voided because of Low Medical Waste Feed Rate. Run 1 was not used in average.

ISOKINETIC SAMPLING TRAIN RESULTS - METHOD

M29

Client Name	Ogden Energy Group, Inc.	Operator	DGB
Plant Name	Lake County Resource Recovery Facility	Project #	10053
Sampling Location	Unit No. 1 FF Outlet	Standard Temperature, °F	88

USE IN AVERAGE OF RUN SET? 1 or 0 ->	0	1	1	1	SET AVERAGE
Run Number	1-O-M29-1	1-O-M29-2	1-O-M29-3	1-O-M29-4	
Run Date	01/27/99	01/27/99	01/27/99	01/27/99	
Run Start Time	hh:mm 840	1140	1420	1713	
Run Stop Time	hh:mm 1111	1350	1648	1920	

Sampling Parameters

Meter Calibration Factor	Y	0.9819	0.9819	0.9819	0.9819	
Pitot Tube Coefficient	C _p	0.84	0.84	0.84	0.84	
Stack/Duct Static Pressure	in H ₂ O	-15.70	-15.70	-15.70	-15.70	-15.70
Stack Cross-Sectional Area	ft ²	17.36	17.36	17.36	17.36	17.36
Barometric Pressure	in Hg	30.3	30.3	30.3	30.3	30.3
Actual Nozzle Diameter	in	0.218	0.218	0.218	0.218	
Carbon Dioxide Percentage	% CO ₂	7.7	7.7	8.3	7.8	7.9
Oxygen Percentage	% O ₂	12.1	12.1	11.4	12.0	11.8
Carbon Monoxide Percentage	% CO	0.0	0.0	0.0	0.0	0.0
Nitrogen Percentage	% N ₂	80.2	80.2	80.3	80.2	80.2
Total Water Volume Collected	mL	308.4	299.5	292.2	266.9	286.2
Sample Volume	ft ³	73.716	71.594	74.634	71.502	72.577
Average Meter Temperature	°F	77	83	84	85	84
Average Stack Temperature	°F	277	278	279	278	278
Average Delta H	in H ₂ O	1.20	1.11	1.23	1.10	1.15
Total Sampling Time	min	121.5	121.5	121.5	121.5	121.5

Air Flow Parameters

Volume of Water vapor @ STP	SCF	14.518	14.097	13.754	12.563	13.471
Volume Metered @ STP	DSCF	72.289	69.372	72.176	69.069	70.206
Absolute Stack/Duct Pressure	in Hg	29.1	29.1	29.1	29.1	29.1
Absolute Meter Pressure	in Hg	30.4	30.4	30.4	30.4	30.4
Calculated Stack Moisture	% H ₂ O	16.7	16.9	16.0	15.4	16.1
Reported Stack Moisture Content	% H ₂ O	16.7	16.9	16.0	15.4	16.1
Dry Mole Fraction	decimal	0.833	0.831	0.840	0.846	0.839
Avg Differential Press. (Delta P)	in H ₂ O	0.931	0.838	0.927	0.834	0.867
Dry Gas Molecular Weight	lb/lb-mole	29.72	29.72	29.78	29.73	29.74
Wet Stack Gas Molecular Weight	lb/lb-mole	27.76	27.74	27.90	27.92	27.85
Average Stack Gas Velocity	ft/sec	66.15	62.81	65.92	62.47	63.73
Percent of Isokinetic Rate	% ISO	99.6	100.9	99.1	99.3	99.8

Air Flow Rate Results

Actual Stack Flow/Minute	ACFM	68,897	65,425	68,662	65,066	66,384
Dry Standard Stack Flow/Minute	DSCFM	40,037	37,905	40,147	38,345	38,799

Concentration and Emission Rate Data Summary

Mercury	ug	40083.80	8440.96	2099.86	867.36	3802.73
Concentration ug/DSCM	ug/DSCM	19570	4297	1027	443	1922
Concentration @ ug 12% CO ₂	ug@12%	30498	6696	1485	682	2954
Concentration ug @ 7% O ₂	ug@7%	30911	6787	1503	693	2994
Concentration Gr @ 12% CO ₂	Gr@12%	1.33E-02	2.93E-03	6.49E-04	2.98E-04	1.29E-03
Emission Rate, lb/hr	lb/hr	2.94	0.610	0.155	0.0837	0.276

* Note: Run 1 was voided because of Low Medical Waste Feed Rate. Run 1 was not used in average.

ISOKINETIC SAMPLING TRAIN DATASHEET - METHOD M29

Client Name	Ogden Energy Group, Inc.	Run #	1-I-M29-1		
Plant Name	Lake County Resource Recovery Facility	Project #	10053	Run Start	840
Plant City, State	Okahumpka, Florida	Personnel	WHH, JPD	Run End	1107
Test Location	Unit No. 1 SDA Inlet	Tester Signature	<i>Bill Harris</i>		
Date of Test	01/27/99	Checked By	<i>Angela Simms</i>		

Isokinetic Factor Setup		Pressures		Sampling Equipment		Filter ID & Tares		Actuals
$\Delta H @ 0.75 \text{ SCFM}$	1.896	Pbar	30.3	Meter Console #	T4			CO ₂
Meter Calibration Factor	0.9975	Pstatic	-2.60	Ideal Nozzle Diameter	0.277			8.2
Pitot Tube Coefficient	0.840	Abs P	30.1	Nozzle #	GN161			O ₂
Estimated Dry Gas Meter Temp	70	Tstd, °F	68	Actual Nozzle Diameter	0.218			11.6
Estimated Stack Temp or M2 Avg.	430	Pstd	29.92	Probe Lgth/ID #	5' P163			CO
Estimated Delta P or M2 Avg.	0.600	Estimates		Liner Material	BG	XAD ID & Tares		0.0
Estimated Moisture Content	12.0	CO ₂	7.5	Filter Box #	HB4	NA	NA	N ₂
Estimated Dry Molecular Weight	29.68	O ₂	12.0	Cold Box ID #	CB8			80.2
Estimated Velocity, ft/sec	56.9	CO	0.0	Umbilical ID #	U50-1			H ₂ O
K Factor (delta H/delta P)	1.23	N ₂	80.5	TC ID #s	41			174.3

Equipment & Leak Check Data, OK? Y or N				Leak Checks		1	2	3	4	5	6	Status
Tambient	62	70	PRE	POST	DGM initial							0.000
Thermocouples			OK	OK	Vacuum	15	13					15
Pitots	163		OK	OK	Leak Rate	0.002	0.010					OK
Tedlar Bag	OB-3		OK	OK	DGM final							0.000

Point #	Clock Time		Dry Gas Meter Reading ft ³	Velocity Head in H ₂ O	Desired Orifice ΔH in H ₂ O	Actual Orifice ΔH in H ₂ O	Pump Vac. in Hg	DGM Inlet Temp °F	DGM Outlet Temp °F	Stack Temp °F	Filter Temp °F	Imp. Exit Temp °F	Cond. Exit Temp °F
	24 hr	min											
A - 1	840	0.0	329.749	0.60	0.74	0.78	3	67	66	428	245	61	NA
A - 2		4.5	331.870	0.70	0.86	0.87	4	71	67	438	245	57	NA
A - 3		9.0	334.370	0.68	0.84	0.84	4	73	68	438	245	57	NA
A - 4		13.5	336.310	0.68	0.84	0.84	5	74	69	438	245	56	NA
A - 5		18.0	338.37	0.76	0.94	0.94	6	75	69	444	245	55	NA
A - 6		22.5	340.720	0.73	0.90	0.90	6	75	70	446	245	55	NA
A - 7		27.0	342.950	0.64	0.79	0.79	6	77	71	444	245	59	NA
A - 8		31.5	345.100	0.71	0.87	0.87	7	77	72	442	248	59	NA
A - 9		36.0	347.420	0.67	0.82	0.82	7	77	72	440	248	59	NA
B - 9	937	40.5	349.610	0.40	0.49	0.49	7	75	74	430	248	62	NA
B - 8		45.0	351.320	0.57	0.70	0.70	7	74	72	432	242	57	NA
B - 7		49.5	353.400	0.52	0.64	0.64	7	74	72	432	242	54	NA
B - 6		54.0	355.340	0.53	0.65	0.65	8	75	72	434	247	54	NA
B - 5		58.5	357.320	0.49	0.60	0.60	8	77	72	433	248	54	NA
B - 4		63.0	359.240	0.55	0.68	0.68	8	77	73	431	249	54	NA
B - 3		67.5	361.310	0.59	0.73	0.73	9	78	73	427	249	54	NA
B - 2		72.0	363.350	0.64	0.79	0.79	10	78	74	434	242	55	NA
B - 1		76.5	365.540	0.68	0.84	0.84	11	79	74	443	242	56	NA
C - 9		81.0	367.732	0.44	0.54	0.54	8	78	74	436	245	60	NA
C - 8		85.5	369.600	0.52	0.64	0.64	9	79	75	442	245	58	NA
C - 7		90.0	371.470	0.68	0.84	0.84	11	80	75	446	245	57	NA
C - 6		94.5	373.690	0.60	0.74	0.74	11	81	75	441	245	56	NA
C - 5		99.0	375.770	0.60	0.74	0.74	12	81	76	438	241	57	NA
C - 4		103.5	377.850	0.72	0.89	0.89	13	83	77	450	241	58	NA
C - 3		108.0	379.890	0.65	0.80	0.80	12	83	78	444	242	61	NA

Continued on Page 2

ISOKINETIC SAMPLING TRAIN DATASHEET - METHOD M29

Client Name	Ogden Energy Group, Inc.	Run #	1-O-M29-1		
Plant Name	Lake County Resource Recovery Facility	Project #	10053	Run Start	840
Plant City, State	Okahumpka, Florida	Personnel	DGB	Run End	1111
Test Location	Unit No. 1 FF Outlet	Tester Signature	<i>David L. Brittle</i>		
Date of Test	01/27/99	Checked By	<i>Shayla...</i>		

Isokinetic Factor Setup		Pressures		Sampling Equipment		Filter ID & Tares		Actuals
ΔH @ 0.75 SCFM	1.818	Pbar	30.3	Meter Console #	T2	Quartz	NA	CO ₂
Meter Calibration Factor	0.9819	Pstatic	-15.70	Ideal Nozzle Diameter	0.246			7.7
Pitot Tube Coefficient	0.840	Abs P	29.1	Nozzle #	GN162			O ₂
Estimated Dry Gas Meter Temp	75	Tstd, °F	68	Actual Nozzle Diameter	0.218			12.1
Estimated Stack Temp or M2 Avg.	280	Pstd	29.92	Probe Lgth/ID #	5' P164			CO
Estimated Delta P or M2 Avg.	0.900	Estimates		Liner Material	BG	XAD ID & Tares		0.0
Estimated Moisture Content	16.0	CO ₂	8.0	Filter Box #	HB1	NA	NA	N ₂
Estimated Dry Molecular Weight	29.76	O ₂	12.0	Cold Box ID #	CB10			80.2
Estimated Velocity, ft/sec	65.0	CO	0.0	Umbilical ID #	U50-1			H ₂ O
K Factor (delta H/delta P)	1.29	N ₂	80.0	TC ID #s	7			308.4

Equipment & Leak Check Data, OK? Y or N				Leak Checks		1	2	3	4	5	6	Status
Tambient	61	80	PRE	POST	DGM initial		908.910	912.051	935.946	949.468		3706.375
Thermocouples			Y	Y	Vacuum	10					8	10
Pitots			Y	Y	Leak Rate	0.005					0.001	OK
Tedlar Bag		OB2	Y	Y	DGM final		909.020	912.230	936.041	949.545		3706.836

Point #	Clock Time	Test Time	Dry Gas Meter Reading	Velocity Head	Desired	Actual	Pump Vac.	DGM Inlet Temp	DGM Outlet Temp	Stack Temp	Filter Temp	Imp. Exit Temp	Cond. Exit Temp
					Orifice ΔH	Orifice ΔH							
	24 hr	min	ft ³	in H ₂ O	in H ₂ O	in H ₂ O	in Hg	°F	°F	°F	°F	°F	°F
A - 9	840	0.0	887.190	1.15	1.48	1.48	5	68	68	276	248	55	NA
A - 8		4.5	890.170	1.10	1.41	1.41	5	68	69	278	252	47	NA
A - 7		9.0	892.760	1.25	1.61	1.61	6	68	69	278	249	52	NA
A - 6		13.5	895.850	1.10	1.41	1.41	5	69	69	281	249	49	NA
A - 5		18.0	898.830	0.98	1.26	1.26	5	71	69	279	248	51	NA
A - 4		22.5	901.620	0.87	1.12	1.12	5	72	70	275	248	52	NA
A - 3		27.0	904.270	0.83	1.07	1.07	5	73	71	275	249	52	NA
A - 2		31.5	906.840	0.85	1.09	1.09	5	74	71	274	249	53	NA
A - 1		36.0	909.660	0.68	0.87	0.87	4	74	72	273	246	56	NA
B - 9	941	40.5	912.051	0.98	1.26	1.26	5	75	73	275	246	57	NA
B - 8		45.0	914.980	0.87	1.12	1.12	5	77	74	275	249	53	NA
B - 7		49.5	917.650	0.75	0.96	0.96	4	78	74	277	250	53	NA
B - 6		54.0	920.160	0.80	1.03	1.03	5	80	75	276	250	54	NA
B - 5		58.5	922.760	0.76	0.98	0.98	4	81	75	277	251	54	NA
B - 4		63.0	925.290	0.80	1.03	1.03	5	82	77	275	251	53	NA
B - 3		67.5	927.830	0.88	1.13	1.13	5	83	77	279	251	53	NA
B - 2		72.0	930.540	0.92	1.18	1.18	5	84	78	281	250	53	NA
B - 1		76.5	933.260	0.88	1.13	1.13	5	83	78	282	251	54	NA
C - 9	1024	81.0	935.946	1.05	1.35	1.35	6	83	79	278	251	55	NA
C - 8		85.5	938.920	1.12	1.44	1.44	6	85	80	281	249	52	NA
C - 7		90.0	941.850	0.97	1.25	1.25	5	85	81	278	249	52	NA
C - 6		94.5	944.330	0.81	1.04	1.04	5	84	81	278	249	53	NA
C - 5		99.0	947.260	1.03	1.32	1.32	6	84	81	274	249	54	NA
C - 4		103.5	950.040	1.02	1.31	1.31	6	81	81	276	251	54	NA
C - 3		108.0	952.910	1.10	1.41	1.41	6	82	81	278	250	54	NA

Continued on Page 2



DATE RECEIVED 02-01-99 Analytical and Consulting Chemists
 DATE REPORTED 02-24-99 1316 South Fifth Street
 99W9412 Wilmington, N.C. 28401
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PAGE 1 OF 1

TESTAR INC
 7424-108 ACC BLVD
 RALEIGH, NC 27613

P.O. # 10053-64

ATTENTION: DAVID BRINTLE

SAMPLE DESCRIPTION: M29 Hg

1. 1-1-M29-1
2. 1-O-M29-1
3. METHOD SW846-

RESULTS

	<u>1</u>	<u>2</u>	<u>3</u>
RESULTS FOR MERCURY TOTAL UG			
Mercury, Front 1/2, Total ug	3770	39.3	7470
Mercury, Front 1/2, Total ug	3840	38.9	7470
Mercury, Back 1/2, Total ug	49600	39800	7470
Mercury, Back 1/2, Total ug	49800	39900	7470
Mercury, HN03, Total ug	17.6	16.3	7470
Mercury, HN03, Total ug	17.4	16.2	7470
Mercury, KMn04, Total ug	648	88.3	7470
Mercury, KMn04, Total ug	653	89.8	7470
Mercury, HCl, Total ug	240	70.0	7470
Mercury, HCl, Total ug	238	68.8	7470


 KEN SMITH, SENIOR ANALYST

227A

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 21, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1049.2</u> KLB	STEAM PRODUCED: <u>1542.4</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1071.4</u> KLB	FEEDWATER USED: <u>1576.0</u> KLB	ENDING: <u>8419.0</u> WH TOT	BEGINNING: <u>175835</u> CU FT
		BEGINNING: <u>8411.0</u> WH TOT	ENDING: <u>176133</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	TOTAL: <u>230.4</u> MWH	TOTAL USED: <u>298</u> CU FT
BLOWDOWN: <u>22</u> KLB	BLOWDOWN: <u>34</u> KLB		
BLOWDOWN: <u>2.1</u> %	BLOWDOWN: <u>2.1</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>6014810</u> JEM TOT	ENDING: <u>6.8</u> FT/IN OUT
ENDING: <u>74306.8</u> HRS	ENDING: <u>73277.4</u> HRS	BEGINNING: <u>5818950</u> JEM TOT	BEGINNING: <u>6.6</u> FT/IN OUT
BEGINNING: <u>74284.4</u> HRS	BEGINNING: <u>73253.4</u> HRS	TOTAL: <u>195.9</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>22.4</u> HRS	TOTAL: <u>24.0</u> HRS		
		UTILITY IN:	EOM OUT: <u>6.67</u>
BOILER RUN TIME: <u>17.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	
AVG. STEAM FLOW: <u>61.7</u> KLB/HR	AVG. STEAM FLOW: <u>64.3</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>134.0</u> TONS	APPROX REF PROC: <u>212.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #1: <u>391</u> LBS
REFUSE PROCESSED: <u>174.9</u> TONS	REFUSE PROCESSED: <u>257.1</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	USAGE UNIT #2: <u>552</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>34.5</u> MWH	DAILY TOTAL: <u>943</u> LBS
		KWH/TON: <u>97.2</u>	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2591.6</u> KLB	GROSS REFUSE REC: <u>565.55</u> TONS		ENDING: <u>12</u> FT. OUT <u>98</u> IN OUT
TOTAL REFUSE PR. <u>355.3</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>13</u> FT. OUT <u>0</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>565.55</u> TONS		EOM OUT: <u>20.17</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,800.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>416895000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>9.27</u> TONS	
BEGINNING: <u>416690000</u> GAL		% OF REFUSE PROC: <u>2.61</u> %	
TOTAL USED: <u>205000</u> GAL			
UNIT 1 AVAILABILITY: <u>70.8</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>67.9</u> %	UNIT 2 % MCR: <u>99.8</u> %	TG % MCR: <u>61.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>11.2</u>	GROSS KW/TON PR. <u>648.5</u>	
NET KWH/TON PR. <u>551.3</u>	LB LIME/TON PR.: <u>1.8</u>	TOT STM TO T/G: <u>2,356.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler off line 7 hours to repair economizer rupture tube leaks.

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OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE April 22, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1362.2</u> KLB	STEAM PRODUCED: <u>1518.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1421.3</u> KLB	FEEDWATER USED: <u>1553.9</u> KLB	ENDING: <u>8429.0</u> WH TOT	BEGINNING: <u>176133</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8419.0</u> WH TOT	ENDING: <u>176133</u> CU FT
BLOWDOWN: <u>59</u> KLB	BLOWDOWN: <u>36</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>4.2</u> %	BLOWDOWN: <u>2.3</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>6251300</u> JEM TOT	ENDING: <u>7.0</u> FT/IN OUT
ENDING: <u>74330.8</u> HRS	ENDING: <u>73301.2</u> HRS	BEGINNING: <u>6014810</u> JEM TOT	BEGINNING: <u>6.8</u> FT/IN OUT
BEGINNING: <u>74306.8</u> HRS	BEGINNING: <u>73277.4</u> HRS	TOTAL: <u>236.5</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.8</u> HRS	UTILITY IN:	EOM OUT: <u>7.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>56.8</u> KLB/HR	AVG. STEAM FLOW: <u>63.2</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>200.0</u> TONS	APPROX REF PROC: <u>220.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>227.0</u> TONS	REFUSE PROCESSED: <u>253.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>51.5</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>122.1</u>	ENDING: <u>12</u> FT. OUT <u>73</u> IN OUT
TOTAL STEAM FLOW: <u>2880.2</u> KLB	GROSS REFUSE REC: <u>184.97</u> TONS		BEGINNING: <u>12</u> FT. OUT <u>98</u> IN OUT
TOTAL REFUSE PR: <u>421.9</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS		EOM OUT: <u>18.08</u>
	TOTAL REFUSE REC: <u>184.97</u> TONS		
WELL WATER USE:	EST PIT INVENTORY: <u>2,397.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>417122000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>1.87</u> TONS	
BEGINNING: <u>416895000</u> GAL		% OF REFUSE PROC: <u>0.44</u> %	
TOTAL USED: <u>227000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>88.1</u> %	UNIT 2 % MCR: <u>98.2</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR: <u>3.0</u>	LB STEAM/GROSS KW: <u>10.0</u>	GROSS KW/TON PR: <u>682.7</u>	
NET KWH/TON PR: <u>560.6</u>	LB LIME/TON PR.: <u>1.5</u>	TOT STM TO T/G: <u>2,838.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE April 23, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1144.0</u> KLB	STEAM PRODUCED: <u>1130.3</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1186.9</u> KLB	FEEDWATER USED: <u>1162.4</u> KLB	ENDING: <u>8436.0</u> WH TOT	BEGINNING: <u>176133</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8429.0</u> WH TOT	ENDING: <u>176209</u> CU FT
BLOWDOWN: <u>43</u> KLB	BLOWDOWN: <u>32</u> KLB	TOTAL: <u>201.6</u> MWH	TOTAL USED: <u>76</u> CU FT
BLOWDOWN: <u>3.6</u> %	BLOWDOWN: <u>2.8</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>6416850</u> JEM TOT	ENDING: <u>8.1</u> FT/IN OUT
ENDING: <u>74354.8</u> HRS	ENDING: <u>73325.1</u> HRS	BEGINNING: <u>6251300</u> JEM TOT	BEGINNING: <u>7.0</u> FT/IN OUT
BEGINNING: <u>74330.8</u> HRS	BEGINNING: <u>73301.2</u> HRS	TOTAL: <u>165.6</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.9</u> HRS	UTILITY IN:	EOM OUT: <u>8.08</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>47.7</u> KLB/HR	AVG. STEAM FLOW: <u>47.1</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>608</u> LBS
APPROX REF PROC: <u>189.0</u> TONS	APPROX REF PROC: <u>190.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>608</u> LBS
REFUSE PROCESSED: <u>190.7</u> TONS	REFUSE PROCESSED: <u>188.4</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1216</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>36.0</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2274.3</u> KLB	GROSS REFUSE REC: <u>59.78</u> TONS	KWH/TON: <u>95.1</u>	ENDING: <u>12</u> FT. OUT <u>5</u> IN OUT
TOTAL REFUSE PR. <u>379.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>12</u> FT. OUT <u>73</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>13.29</u> TONS		RECEIVED: <u>0.00</u> TONS
ENDING: <u>417424000</u> GAL	TOTAL REFUSE REC: <u>46.49</u> TONS	MEDICAL WASTE:	EOM OUT: <u>12.42</u>
BEGINNING: <u>417122000</u> GAL	EST PIT INVENTORY: <u>1,808.0</u> TONS	PROCESSED: <u>0.00</u> TONS	
TOTAL USED: <u>302000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>74.0</u> %	UNIT 2 % MCR: <u>73.1</u> %	TG % MCR: <u>53.5</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>11.3</u>	GROSS KW/TON PR. <u>531.9</u>	
NET KWH/TON PR. <u>436.8</u>	LB LIME/TON PR.: <u>9.1</u>	TOT STM TO T/G: <u>2,061.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 24, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1180.8</u> KLB	STEAM PRODUCED: <u>1259.1</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1222.8</u> KLB	FEEDWATER USED: <u>1292.9</u> KLB	ENDING: <u>8444.0</u> WH TOT	BEGINNING: <u>176209</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8436.0</u> WH TOT	ENDING: <u>176882</u> CU FT
BLOWDOWN: <u>42</u> KLB	BLOWDOWN: <u>34</u> KLB	TOTAL: <u>230.4</u> MWH	TOTAL USED: <u>473</u> CU FT
BLOWDOWN: <u>3.4</u> %	BLOWDOWN: <u>2.6</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>6801130</u> JEM TOT	ENDING: <u>8.3</u> FT/IN OUT
ENDING: <u>74369.3</u> HRS	ENDING: <u>73349.0</u> HRS	BEGINNING: <u>6416850</u> JEM TOT	BEGINNING: <u>8.1</u> FT/IN OUT
BEGINNING: <u>74354.8</u> HRS	BEGINNING: <u>73325.1</u> HRS	TOTAL: <u>184.3</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>14.5</u> HRS	TOTAL: <u>23.9</u> HRS	UTILITY IN:	EOM OUT: <u>8.21</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>49.2</u> KLB/HR	AVG. STEAM FLOW: <u>52.5</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>720</u> LBS
APPROX REF PROC: <u>210.0</u> TONS	APPROX REF PROC: <u>207.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>720</u> LBS
REFUSE PROCESSED: <u>196.8</u> TONS	REFUSE PROCESSED: <u>209.9</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1440</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>45.1</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2439.9</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS	KWH/TON: <u>113.4</u>	ENDING: <u>11</u> FT. OUT <u>85</u> IN OUT
TOTAL REFUSE PR. <u>406.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>12</u> FT. OUT <u>5</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>0.00</u> TONS		EOM OUT: <u>18.08</u>
WELL WATER USE:	EST PIT INVENTORY: <u>1,108.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>417713000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>417424000</u> GAL		% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>289000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>76.4</u> %	UNIT 2 % MCR: <u>81.5</u> %	TG % MCR: <u>61.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.6</u>	GROSS KW/TON PR. <u>566.6</u>	
NET KWH/TON PR. <u>453.2</u>	LB LIME/TON PR.: <u>1.2</u>	TOT STM TO T/G: <u>2,267.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 25, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1283.5</u> KLB	STEAM PRODUCED: <u>1323.5</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1326.5</u> KLB	FEEDWATER USED: <u>1354.1</u> KLB	ENDING: <u>8453.0</u> WH TOT	BEGINNING: <u>176682</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8444.0</u> WH TOT	ENDING: <u>177641</u> CU FT
BLOWDOWN: <u>43</u> KLB	BLOWDOWN: <u>31</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>859</u> CU FT
BLOWDOWN %: <u>3.2</u> %	BLOWDOWN %: <u>2.3</u> %	UTILITY OUT:	
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>6809930</u> JEM TOT	PEBBLE LIME:
ENDING: <u>74393.3</u> HRS	ENDING: <u>73372.9</u> HRS	BEGINNING: <u>6801130</u> JEM TOT	ENDING: <u>9.8</u> FT/IN OUT
BEGINNING: <u>74369.3</u> HRS	BEGINNING: <u>73349.0</u> HRS	TOTAL: <u>208.8</u> MWH	BEGINNING: <u>8.3</u> FT/IN OUT
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.9</u> HRS		RECEIVED: <u>0.00</u> TONS
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.67</u>
AVG. STEAM FLOW: <u>53.5</u> KLB/HR	AVG. STEAM FLOW: <u>55.1</u> KLB/HR	ENDING: <u>2722250</u> JEM TOT	
APPROX REF PROC: <u>192.0</u> TONS	APPROX REF PROC: <u>201.0</u> TONS	BEGINNING: <u>2722250</u> JEM TOT	CARBON USAGE:
REFUSE PROCESSED: <u>213.9</u> TONS	REFUSE PROCESSED: <u>220.6</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #1: <u>720</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	USAGE UNIT #2: <u>720</u> LBS
TOTAL STEAM FLOW: <u>2607.0</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS	IN PLANT USE: <u>50.4</u> MWH	DAILY TOTAL: <u>1440</u> LBS
TOTAL REFUSE PR. <u>393.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>128.2</u>	CARBON INVENTORY:
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		ENDING: <u>11</u> FT. OUT <u>82</u> IN OUT
ENDING: <u>418003000</u> GAL	TOTAL REFUSE REC: <u>0.00</u> TONS	MEDICAL WASTE:	BEGINNING: <u>11</u> FT. OUT <u>85</u> IN OUT
BEGINNING: <u>417713000</u> GAL	EST PIT INVENTORY: <u>933.0</u> TONS	PROCESSED: <u>0.00</u> TONS	RECEIVED: <u>0.00</u> TONS
TOTAL USED: <u>290000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.00</u> %	EOM OUT: <u>17.83</u>
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>83.0</u> %	UNIT 2 % MCR: <u>85.6</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.1</u>	GROSS KW/TON PR. <u>659.5</u>	
NET KWH/TON PR. <u>531.3</u>	LB LIME/TON PR.: <u>12.0</u>	TOT STM TO T/G: <u>2,595.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE APRIL 28, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1255.0</u> KLB	STEAM PRODUCED: <u>1289.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1297.0</u> KLB	FEEDWATER USED: <u>1322.0</u> KLB	ENDING: <u>8461.0</u> WH TOT	BEGINNING: <u>177641</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8453.0</u> WH TOT	ENDING: <u>179897</u> CU FT
BLOWDOWN: <u>42</u> KLB	BLOWDOWN: <u>33</u> KLB	TOTAL: <u>230.4</u> MWH	TOTAL USED: <u>2256</u> CU FT
BLOWDOWN: <u>3.2</u> %	BLOWDOWN: <u>2.5</u> %	UTILITY OUT:	
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>7010500</u> JEM TOT	PEBBLE LIME:
ENDING: <u>74417.1</u> HRS	ENDING: <u>73394.8</u> HRS	BEGINNING: <u>6809930</u> JEM TOT	ENDING: <u>12.0</u> FT/IN OUT
BEGINNING: <u>74393.3</u> HRS	BEGINNING: <u>73372.9</u> HRS	TOTAL: <u>200.6</u> MWH	BEGINNING: <u>9.8</u> FT/IN OUT
TOTAL: <u>23.8</u> HRS	TOTAL: <u>21.9</u> HRS		RECEIVED: <u>0.00</u> TONS
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>12.00</u>
AVG. STEAM FLOW: <u>52.3</u> KLB/HR	AVG. STEAM FLOW: <u>53.7</u> KLB/HR	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>131.0</u> TONS	APPROX REF PROC: <u>134.0</u> TONS	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>720</u> LBS
REFUSE PROCESSED: <u>209.2</u> TONS	REFUSE PROCESSED: <u>214.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>720</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1440</u> LBS
TOTAL STEAM FLOW: <u>2544.0</u> KLB	GROSS REFUSE REC: <u>64.75</u> TONS	IN PLANT USE: <u>29.8</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>267.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>111.5</u>	ENDING: <u>11</u> FT. OUT <u>75</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS	MEDICAL WASTE:	BEGINNING: <u>11</u> FT. OUT <u>82</u> IN OUT
ENDING: <u>418291000</u> GAL	TOTAL REFUSE REC: <u>64.75</u> TONS	PROCESSED: <u>2.48</u> TONS	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>418003000</u> GAL	EST PIT INVENTORY: <u>788.0</u> TONS	% OF REFUSE PROC: <u>0.93</u> %	EOM OUT: <u>17.25</u>
TOTAL USED: <u>288000</u> GAL	ASH HAULED: <u>0.00</u> TONS		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>81.2</u> %	UNIT 2 % MCR: <u>83.4</u> %	TG % MCR: <u>61.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>11.0</u>	GROSS KW/TON PR. <u>861.4</u>	
NET KWH/TON PR. <u>749.9</u>	LB LIME/TON PR.: <u>25.8</u>	TOT STM TO T/G: <u>2,461.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE APRIL 27, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1307.0</u> KLB	STEAM PRODUCED: <u>1328.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1351.0</u> KLB	FEEDWATER USED: <u>1387.0</u> KLB	ENDING: <u>8470.0</u> WH TOT	BEGINNING: <u>179897</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8461.0</u> WH TOT	ENDING: <u>180520</u> CU FT
BLOWDOWN: <u>44</u> KLB	BLOWDOWN: <u>39</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>623</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>2.9</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>7221610</u> JEM TOT	ENDING: <u>12.8</u> FT/IN OUT
ENDING: <u>74441.1</u> HRS	ENDING: <u>73418.7</u> HRS	BEGINNING: <u>7010500</u> JEM TOT	BEGINNING: <u>12.0</u> FT/IN OUT
BEGINNING: <u>74417.1</u> HRS	BEGINNING: <u>73394.8</u> HRS	TOTAL: <u>211.1</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.9</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>12.67</u>
AVG. STEAM FLOW: <u>54.5</u> KLB/HR	AVG. STEAM FLOW: <u>55.3</u> KLB/HR	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>209.0</u> TONS	APPROX REF PROC: <u>171.4</u> TONS	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>720</u> LBS
REFUSE PROCESSED: <u>217.8</u> TONS	REFUSE PROCESSED: <u>221.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>720</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1440</u> LBS
TOTAL STEAM FLOW: <u>2635.0</u> KLB	GROSS REFUSE REC: <u>662.63</u> TONS	IN PLANT USE: <u>48.1</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR: <u>385.6</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>124.7</u>	ENDING: <u>11</u> FT. OUT <u>20</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		BEGINNING: <u>11</u> FT. OUT <u>75</u> IN OUT
ENDING: <u>418593000</u> GAL	TOTAL REFUSE REC: <u>662.63</u> TONS	MEDICAL WASTE:	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>418291000</u> GAL	EST PIT INVENTORY: <u>1,669.0</u> TONS	PROCESSED: <u>5.23</u> TONS	EOM OUT: <u>12.67</u>
TOTAL USED: <u>302000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.36</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>84.6</u> %	UNIT 2 % MCR: <u>85.9</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR: <u>3.0</u>	LB STEAM/GROSS KW: <u>10.2</u>	GROSS KW/TON PR: <u>672.2</u>	
NET KWH/TON PR: <u>547.5</u>	LB LIME/TON PR.: <u>6.5</u>	TOT STM TO T/G: <u>2,607.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 28, 1999

BOILER NO. 1

STEAM PRODUCED: 1385.0 KLB
FEEDWATER USED: 1433.0 KLB

BOILER BLOWDOWN:
BLOWDOWN: 48 KLB
BLOWDOWN: 3.3 %

GRATE RUN TIME:
ENDING: 74465.1 HRS
BEGINNING: 74441.1 HRS
TOTAL: 24.0 HRS

BOILER RUN TIME: 24.0 HRS

AVG. STEAM FLOW: 57.7 KLB/HR

APPROX REF PROC: 200.0 TONS

REFUSE PROCESSED: 230.8 TONS

NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB

TOTAL STEAM FLOW: 2836.0 KLB
TOTAL REFUSE PR. 439.4 TONS

WELL WATER USE:
ENDING: 418881000 GAL
BEGINNING: 418593000 GAL
TOTAL USED: 288000 GAL

UNIT 1 AVAILABILITY: 100.0 %
UNIT 1 % MCR: 89.6 %
LB STEAM/LB PR. 3.0
NET KWH/TON PR. 530.9

BOILER NO. 2

STEAM PRODUCED: 1451.0 KLB
FEEDWATER USED: 1494.0 KLB

BOILER BLOWDOWN:
BLOWDOWN: 43 KLB
BLOWDOWN: 2.9 %

GRATE RUN TIME:
ENDING: 73442.7 HRS
BEGINNING: 73418.7 HRS
TOTAL: 24.0 HRS

BOILER RUN TIME: 24.0 HRS

AVG. STEAM FLOW: 60.5 KLB/HR

APPROX REF PROC: 226.0 TONS

REFUSE PROCESSED: 241.8 TONS

GROSS REFUSE REC: 436.51 TONS
NON PROCESSED: 0.00 TONS
FERROUS HAULED: 0.00 TONS
TOTAL REFUSE REC: 436.51 TONS

EST PIT INVENTORY: 1,848.0 TONS
ASH HAULED: 0.00 TONS

UNIT 2 AVAILABILITY: 100.0 %
UNIT 2 % MCR: 93.9 %
LB STEAM/GROSS KW 9.8
LB LIME/TON PR.: 83.4

ELECTRICITY

GENERATOR OUT:
ENDING: 8480.0 WH TOT
BEGINNING: 8470.0 WH TOT
TOTAL: 288.0 MWH

UTILITY OUT:
ENDING: 7454870 JEM TOT
BEGINNING: 7221610 JEM TOT
TOTAL: 233.3 MWH

UTILITY IN:
ENDING: 2722250 JEM TOT
BEGINNING: 2722250 JEM TOT
TOTAL: 0.0 MWH

GENERATOR RUN TIME: 24.0 HRS
IN PLANT USE: 54.7 MWH
KWH/TON: 124.6

MEDICAL WASTE :
PROCESSED: 13.37 TONS
% OF REFUSE PROC: 3.04 %

TG AVAILABILITY: 100.0 %
TG % MCR: 76.4 %
GROSS KW/TON PR. 655.5
TOT STM TO T/G: 2,821.0

INVENTORY

NATURAL GAS USAGE:
BEGINNING: 180520 CU FT
ENDING: 180528 CU FT
TOTAL USED: 8 CU FT

PEBBLE LIME :
ENDING: 9.1 FT/IN OUT
BEGINNING: 12.8 FT/IN OUT
RECEIVED: 24.12 TONS

EOM OUT: 9.08

CARBON USAGE:
USAGE UNIT #1: 720 LBS
USAGE UNIT #2: 720 LBS

DAILY TOTAL: 1440 LBS

CARBON INVENTORY:
ENDING: 10 FT. OUT 70 IN OUT
BEGINNING: 11 FT. OUT 20 IN OUT
RECEIVED: 0.00 TONS

EOM OUT: 15.83

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE APRIL 29, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1429.0</u> KLB	STEAM PRODUCED: <u>1458.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1462.0</u> KLB	FEEDWATER USED: <u>1531.0</u> KLB	ENDING: <u>8490.0</u> WH TOT	BEGINNING: <u>180528</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8480.0</u> WH TOT	ENDING: <u>180528</u> CU FT
BLOWDOWN: <u>53</u> KLB	BLOWDOWN: <u>73</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.6</u> %	BLOWDOWN: <u>4.8</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>7693750</u> JEM TOT	ENDING: <u>9.8</u> FT/IN OUT
ENDING: <u>74489.1</u> HRS	ENDING: <u>73466.8</u> HRS	BEGINNING: <u>7454870</u> JEM TOT	BEGINNING: <u>9.1</u> FT/IN OUT
BEGINNING: <u>74465.1</u> HRS	BEGINNING: <u>73442.7</u> HRS	TOTAL: <u>238.9</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.1</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.67</u>
AVG. STEAM FLOW: <u>59.5</u> KLB/HR	AVG. STEAM FLOW: <u>60.8</u> KLB/HR	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>202.8</u> TONS	APPROX REF PROC: <u>222.8</u> TONS	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>720</u> LBS
REFUSE PROCESSED: <u>238.2</u> TONS	REFUSE PROCESSED: <u>243.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>720</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1440</u> LBS
TOTAL STEAM FLOW: <u>2887.0</u> KLB	GROSS REFUSE REC: <u>601.00</u> TONS	IN PLANT USE: <u>49.1</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>436.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>112.5</u>	ENDING: <u>22</u> FT. OUT <u>63</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		BEGINNING: <u>10</u> FT. OUT <u>70</u> IN OUT
ENDING: <u>419189000</u> GAL	TOTAL REFUSE REC: <u>601.00</u> TONS	MEDICAL WASTE:	RECEIVED: <u>20.17</u> TONS
BEGINNING: <u>418881000</u> GAL	EST PIT INVENTORY: <u>1,968.0</u> TONS	PROCESSED: <u>10.90</u> TONS	EOM OUT: <u>27.25</u>
TOTAL USED: <u>308000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.50</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>92.5</u> %	UNIT 2 % MCR: <u>94.3</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.0</u>	GROSS KW/TON PR. <u>659.8</u>	
NET KWH/TON PR. <u>547.3</u>	LB LIME/TON PR.: <u>5.0</u>	TOT STM TO T/G: <u>2,884.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 30, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1324.0</u> KLB	STEAM PRODUCED: <u>1348.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1370.0</u> KLB	FEEDWATER USED: <u>1423.0</u> KLB	ENDING: <u>8500.0</u> WH TOT	BEGINNING: <u>180528</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8490.0</u> WH TOT	ENDING: <u>180560</u> CU FT
BLOWDOWN: <u>46</u> KLB	BLOWDOWN: <u>75</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>32</u> CU FT
BLOWDOWN: <u>3.4</u> %	BLOWDOWN: <u>5.3</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>7915050</u> JEM TOT	ENDING: <u>10.2</u> FT/IN OUT
ENDING: <u>74513.1</u> HRS	ENDING: <u>73490.8</u> HRS	BEGINNING: <u>7893750</u> JEM TOT	BEGINNING: <u>9.8</u> FT/IN OUT
BEGINNING: <u>74489.1</u> HRS	BEGINNING: <u>73486.8</u> HRS	TOTAL: <u>221.3</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>10.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.2</u> KLB/HR	AVG. STEAM FLOW: <u>56.2</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>720</u> LBS
APPROX REF PROC: <u>229.0</u> TONS	APPROX REF PROC: <u>223.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>720</u> LBS
REFUSE PROCESSED: <u>220.7</u> TONS	REFUSE PROCESSED: <u>224.7</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1440</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>66.7</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2672.0</u> KLB	GROSS REFUSE REC: <u>696.29</u> TONS	KWH/TON: <u>147.3</u>	ENDING: <u>21</u> FT. OUT <u>88</u> IN OUT
TOTAL REFUSE PR. <u>452.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>22</u> FT. OUT <u>63</u> IN OUT
	FERROUS HAULED: <u>41.16</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>655.13</u> TONS		EOM OUT: <u>28.33</u>
WELL WATER USE:	EST PIT INVENTORY: <u>1,633.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>419469000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>7.40</u> TONS	
BEGINNING: <u>419189000</u> GAL		% OF REFUSE PROC: <u>1.63</u> %	
TOTAL USED: <u>280000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.7</u> %	UNIT 2 % MCR: <u>87.2</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.3</u>	GROSS KW/TON PR. <u>636.1</u>	
NET KWH/TON PR. <u>488.8</u>	LB LIME/TON PR.: <u>2.8</u>	TOT STM TO T/G: <u>2,682.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 1, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1346.0</u> KLB	STEAM PRODUCED: <u>1294.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1391.0</u> KLB	FEEDWATER USED: <u>1388.0</u> KLB	ENDING: <u>8509.0</u> WH TOT	BEGINNING: <u>180560</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8500.0</u> WH TOT	ENDING: <u>180609</u> CU FT
BLOWDOWN: <u>45</u> KLB	BLOWDOWN: <u>75</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>49</u> CU FT
BLOWDOWN: <u>3.2</u> %	BLOWDOWN: <u>5.5</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>8133750</u> JEM TOT	ENDING: <u>10.8</u> FT/IN OUT
ENDING: <u>74533.1</u> HRS	ENDING: <u>73514.8</u> HRS	BEGINNING: <u>7915050</u> JEM TOT	BEGINNING: <u>10.2</u> FT/IN OUT
BEGINNING: <u>74513.1</u> HRS	BEGINNING: <u>73490.8</u> HRS	TOTAL: <u>218.7</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>20.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>10.67</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>56.1</u> KLB/HR	AVG. STEAM FLOW: <u>53.9</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>720</u> LBS
APPROX REF PROC: <u>254.4</u> TONS	APPROX REF PROC: <u>247.5</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>720</u> LBS
REFUSE PROCESSED: <u>224.3</u> TONS	REFUSE PROCESSED: <u>215.7</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1440</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>40.5</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2640.0</u> KLB	GROSS REFUSE REC: <u>249.07</u> TONS	KWH/TON: <u>89.6</u>	ENDING: <u>21</u> FT. OUT <u>83</u> IN OUT
TOTAL REFUSE PR. <u>452.2</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>21</u> FT. OUT <u>88</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>249.07</u> TONS		EOM OUT: <u>27.92</u>
WELL WATER USE:	EST PIT INVENTORY: <u>1,880.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>419757000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>12.22</u> TONS	
BEGINNING: <u>419469000</u> GAL		% OF REFUSE PROC: <u>2.70</u> %	
TOTAL USED: <u>288000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>87.1</u> %	UNIT 2 % MCR: <u>83.7</u> %	TG % MCR: <u>88.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>573.2</u>	
NET KWH/TON PR. <u>483.6</u>	LB LIME/TON PR.: <u>4.2</u>	TOT STM TO T/G: <u>2,656.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 2, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1335.0</u> KLB	STEAM PRODUCED: <u>1317.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1381.0</u> KLB	FEEDWATER USED: <u>1386.0</u> KLB	ENDING: <u>8518.0</u> WH TOT	BEGINNING: <u>180560</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8509.0</u> WH TOT	ENDING: <u>180689</u> CU FT
BLOWDOWN: <u>46</u> KLB	BLOWDOWN: <u>69</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>129</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>5.0</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>8354300</u> JEM TOT	ENDING: <u>11.2</u> FT/IN OUT
ENDING: <u>74542.3</u> HRS	ENDING: <u>73538.8</u> HRS	BEGINNING: <u>8133750</u> JEM TOT	BEGINNING: <u>10.8</u> FT/IN OUT
BEGINNING: <u>74533.1</u> HRS	BEGINNING: <u>73514.8</u> HRS	TOTAL: <u>220.6</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>9.2</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>11.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.6</u> KLB/HR	AVG. STEAM FLOW: <u>54.9</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>720</u> LBS
APPROX REF PROC: <u>267.0</u> TONS	APPROX REF PROC: <u>263.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>720</u> LBS
REFUSE PROCESSED: <u>222.5</u> TONS	REFUSE PROCESSED: <u>219.5</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1440</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>38.6</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2652.0</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS	KWH/TON: <u>87.1</u>	ENDING: <u>21</u> FT. OUT <u>66</u> IN OUT
TOTAL REFUSE PR. <u>443.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>21</u> FT. OUT <u>83</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS	MEDICAL WASTE:	RECEIVED: <u>0.00</u> TONS
ENDING: <u>420043000</u> GAL	TOTAL REFUSE REC: <u>0.00</u> TONS	PROCESSED: <u>1.73</u> TONS	EOM OUT: <u>26.50</u>
BEGINNING: <u>419757000</u> GAL	EST PIT INVENTORY: <u>1,358.0</u> TONS	% OF REFUSE PROC: <u>0.39</u> %	
TOTAL USED: <u>286000</u> GAL	ASH HAULED: <u>0.00</u> TONS		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>86.4</u> %	UNIT 2 % MCR: <u>85.2</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>584.1</u>	
NET KWH/TON PR. <u>497.0</u>	LB LIME/TON PR.: <u>2.8</u>	TOT STM TO T/G: <u>2,840.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 3 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1414.6</u> KLB	STEAM PRODUCED: <u>1409.2</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1462.5</u> KLB	FEEDWATER USED: <u>1450.8</u> KLB	ENDING: <u>8528.0</u> WH TOT	BEGINNING: <u>180689</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8518.0</u> WH TOT	ENDING: <u>180795</u> CU FT
BLOWDOWN: <u>48</u> KLB	BLOWDOWN: <u>42</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>106</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>2.9</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>8589570</u> JEM TOT	ENDING: <u>12.0</u> FT/IN OUT
ENDING: <u>74566.3</u> HRS	ENDING: <u>73562.8</u> HRS	BEGINNING: <u>8354300</u> JEM TOT	BEGINNING: <u>11.2</u> FT/IN OUT
BEGINNING: <u>74542.3</u> HRS	BEGINNING: <u>73538.8</u> HRS	TOTAL: <u>235.3</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>12.00</u>
AVG. STEAM FLOW: <u>58.9</u> KLB/HR	AVG. STEAM FLOW: <u>58.7</u> KLB/HR	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>220.8</u> TONS	APPROX REF PROC: <u>190.3</u> TONS	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>720</u> LBS
REFUSE PROCESSED: <u>235.8</u> TONS	REFUSE PROCESSED: <u>234.9</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>720</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1440</u> LBS
TOTAL STEAM FLOW: <u>2823.8</u> KLB	GROSS REFUSE REC: <u>754.74</u> TONS	IN PLANT USE: <u>52.7</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>422.3</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>124.9</u>	ENDING: <u>21</u> FT. OUT <u>41</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		BEGINNING: <u>21</u> FT. OUT <u>66</u> IN OUT
ENDING: <u>420346000</u> GAL	TOTAL REFUSE REC: <u>754.74</u> TONS	MEDICAL WASTE:	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>420043000</u> GAL	EST PIT INVENTORY: <u>1,692.0</u> TONS	PROCESSED: <u>11.25</u> TONS	EOM OUT: <u>24.42</u>
TOTAL USED: <u>303000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.66</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>91.5</u> %	UNIT 2 % MCR: <u>91.2</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.8</u>	GROSS KW/TON PR. <u>681.9</u>	
NET KWH/TON PR. <u>557.1</u>	LB LIME/TON PR.: <u>5.9</u>	TOT STM TO T/G: <u>2,580.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 4 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1420.2</u> KLB	STEAM PRODUCED: <u>1436.1</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1469.3</u> KLB	FEEDWATER USED: <u>1479.3</u> KLB	ENDING: <u>8538.0</u> WH TOT	BEGINNING: <u>180795</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8528.0</u> WH TOT	ENDING: <u>180803</u> CU FT
BLOWDOWN: <u>49</u> KLB	BLOWDOWN: <u>43</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>8</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>2.9</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>8829480</u> JEM TOT	ENDING: <u>13.2</u> FT/IN OUT
ENDING: <u>74590.3</u> HRS	ENDING: <u>73586.8</u> HRS	BEGINNING: <u>8589570</u> JEM TOT	BEGINNING: <u>12.0</u> FT/IN OUT
BEGINNING: <u>74566.3</u> HRS	BEGINNING: <u>73562.8</u> HRS	TOTAL: <u>239.9</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>13.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.2</u> KLB/HR	AVG. STEAM FLOW: <u>59.8</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>620</u> LBS
APPROX REF PROC: <u>161.2</u> TONS	APPROX REF PROC: <u>169.6</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>604</u> LBS
REFUSE PROCESSED: <u>236.7</u> TONS	REFUSE PROCESSED: <u>239.4</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1224</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>48.1</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2856.3</u> KLB	GROSS REFUSE REC: <u>719.66</u> TONS	KWH/TON: <u>141.5</u>	ENDING: <u>21</u> FT. OUT <u>10</u> IN OUT
TOTAL REFUSE PR. <u>339.9</u> TONS	NON PROCESSED: <u>0.00</u> TONS	MEDICAL WASTE :	BEGINNING: <u>21</u> FT. OUT <u>41</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS	PROCESSED: <u>9.07</u> TONS	RECEIVED: <u>0.00</u> TONS
ENDING: <u>420652000</u> GAL	TOTAL REFUSE REC: <u>719.66</u> TONS	% OF REFUSE PROC: <u>2.67</u> %	EOM OUT: <u>21.83</u>
BEGINNING: <u>420346000</u> GAL	EST PIT INVENTORY: <u>2,070.0</u> TONS		
TOTAL USED: <u>306000</u> GAL	ASH HAULED: <u>0.00</u> TONS		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>91.9</u> %	UNIT 2 % MCR: <u>92.9</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.9</u>	GROSS KW/TON PR. <u>847.4</u>	
NET KWH/TON PR. <u>705.9</u>	LB LIME/TON PR.: <u>11.1</u>	TOT STM TO T/G: <u>2,856.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 5, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1426.0</u> KLB	STEAM PRODUCED: <u>1429.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1475.0</u> KLB	FEEDWATER USED: <u>1488.0</u> KLB	ENDING: <u>8548.0</u> WH TOT	BEGINNING: <u>180803</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8538.0</u> WH TOT	ENDING: <u>180803</u> CU FT
BLOWDOWN: <u>49</u> KLB	BLOWDOWN: <u>59</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>4.0</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>9068880</u> JEM TOT	ENDING: <u>9.0</u> FT/IN OUT
ENDING: <u>74614.3</u> HRS	ENDING: <u>73610.8</u> HRS	BEGINNING: <u>8829480</u> JEM TOT	BEGINNING: <u>13.2</u> FT/IN OUT
BEGINNING: <u>74590.3</u> HRS	BEGINNING: <u>73586.8</u> HRS	TOTAL: <u>239.4</u> MWH	RECEIVED: <u>24.57</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.4</u> KLB/HR	AVG. STEAM FLOW: <u>59.5</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>562</u> LBS
APPROX REF PROC: <u>179.7</u> TONS	APPROX REF PROC: <u>167.6</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>237.7</u> TONS	REFUSE PROCESSED: <u>238.2</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1114</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>48.6</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2855.0</u> KLB	GROSS REFUSE REC: <u>579.23</u> TONS	KWH/TON: <u>137.9</u>	ENDING: <u>21</u> FT. OUT <u>0</u> IN OUT
TOTAL REFUSE PR. <u>352.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>21</u> FT. OUT <u>10</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>579.23</u> TONS		EOM OUT: <u>21.00</u>
WELL WATER USE:	EST PIT INVENTORY: <u>1,826.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>420956000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>5.19</u> TONS	
BEGINNING: <u>420652000</u> GAL		% OF REFUSE PROC: <u>1.47</u> %	
TOTAL USED: <u>304000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>92.3</u> %	UNIT 2 % MCR: <u>92.5</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.9</u>	GROSS KW/TON PR. <u>817.1</u>	
NET KWH/TON PR. <u>679.2</u>	LB LIME/TON PR.: <u>102.0</u>	TOT STM TO T/G: <u>2,871.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 6, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1414.0</u> KLB	STEAM PRODUCED: <u>1419.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1462.0</u> KLB	FEEDWATER USED: <u>1482.0</u> KLB	ENDING: <u>8557.0</u> WH TOT	BEGINNING: <u>180803</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8548.0</u> WH TOT	ENDING: <u>180804</u> CU FT
BLOWDOWN: <u>48</u> KLB	BLOWDOWN: <u>63</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN %: <u>3.3</u> %	BLOWDOWN %: <u>4.3</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>9304090</u> JEM TOT	ENDING: <u>9.6</u> FT/IN OUT
ENDING: <u>74638.3</u> HRS	ENDING: <u>73634.8</u> HRS	BEGINNING: <u>9068880</u> JEM TOT	BEGINNING: <u>9.0</u> FT/IN OUT
BEGINNING: <u>74614.3</u> HRS	BEGINNING: <u>73610.8</u> HRS	TOTAL: <u>235.2</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.50</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>58.9</u> KLB/HR	AVG. STEAM FLOW: <u>59.1</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>148.0</u> TONS	APPROX REF PROC: <u>153.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>235.7</u> TONS	REFUSE PROCESSED: <u>236.5</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>24.0</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2833.0</u> KLB	GROSS REFUSE REC: <u>513.00</u> TONS	KWH/TON: <u>78.5</u>	ENDING: <u>20</u> FT. OUT <u>59</u> IN OUT
TOTAL REFUSE PR. <u>305.6</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>21</u> FT. OUT <u>0</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
ENDING: <u>421263000</u> GAL	TOTAL REFUSE REC: <u>513.00</u> TONS	MEDICAL WASTE:	EOM OUT: <u>24.92</u>
BEGINNING: <u>420956000</u> GAL	EST PIT INVENTORY: <u>1,867.0</u> TONS	PROCESSED: <u>4.57</u> TONS	
TOTAL USED: <u>307000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.50</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>91.5</u> %	UNIT 2 % MCR: <u>91.8</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.9</u>	GROSS KW/TON PR. <u>848.3</u>	
NET KWH/TON PR. <u>769.7</u>	LB LIME/TON PR.: <u>6.2</u>	TOT STM TO T/G: <u>2,847.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 7, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1432.0</u> KLB	STEAM PRODUCED: <u>1466.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1479.0</u> KLB	FEEDWATER USED: <u>1509.0</u> KLB	ENDING: <u>8566.0</u> WH TOT	BEGINNING: <u>180804</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8557.0</u> WH TOT	ENDING: <u>180807</u> CU FT
BLOWDOWN: <u>47</u> KLB	BLOWDOWN: <u>43</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>3</u> CU FT
BLOWDOWN: <u>3.2</u> %	BLOWDOWN: <u>2.8</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>9514700</u> JEM TOT	ENDING: <u>10.3</u> FT/IN OUT
ENDING: <u>74662.3</u> HRS	ENDING: <u>73658.8</u> HRS	BEGINNING: <u>9304090</u> JEM TOT	BEGINNING: <u>9.6</u> FT/IN OUT
BEGINNING: <u>74638.3</u> HRS	BEGINNING: <u>73634.8</u> HRS	TOTAL: <u>210.6</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>10.25</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.7</u> KLB/HR	AVG. STEAM FLOW: <u>61.1</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>212.0</u> TONS	APPROX REF PROC: <u>204.0</u> TONS	TOTAL: <u>5.6</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>238.7</u> TONS	REFUSE PROCESSED: <u>244.3</u> TONS	GENERATOR RUN TIME: <u>21.3</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>54.1</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2898.0</u> KLB	GROSS REFUSE REC: <u>627.44</u> TONS	KWH/TON: <u>126.8</u>	ENDING: <u>20</u> FT. OUT <u>17</u> IN OUT
TOTAL REFUSE PR. <u>427.1</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>20</u> FT. OUT <u>59</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>627.44</u> TONS		EOM OUT: <u>21.42</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,130.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>421554000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>11.12</u> TONS	
BEGINNING: <u>421263000</u> GAL		% OF REFUSE PROC: <u>2.60</u> %	
TOTAL USED: <u>291000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>88.8</u> %	
UNIT 1 % MCR: <u>92.7</u> %	UNIT 2 % MCR: <u>94.8</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>11.2</u>	GROSS KW/TON PR. <u>606.9</u>	
NET KWH/TON PR. <u>493.1</u>	LB LIME/TON PR.: <u>5.1</u>	TOT STM TO T/G: <u>2,874.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

T/G off line for 2.7 hours due to lightning.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 8 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1469.5</u> KLB	STEAM PRODUCED: <u>1530.9</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1520.5</u> KLB	FEEDWATER USED: <u>1582.2</u> KLB	ENDING: <u>8576.0</u> WH TOT	BEGINNING: <u>180807</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8566.0</u> WH TOT	ENDING: <u>180807</u> CU FT
BLOWDOWN: <u>51</u> KLB	BLOWDOWN: <u>51</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.4</u> %	BLOWDOWN: <u>3.2</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>9765980</u> JEM TOT	ENDING: <u>11.0</u> FT/IN OUT
ENDING: <u>74686.3</u> HRS	ENDING: <u>73682.8</u> HRS	BEGINNING: <u>9514700</u> JEM TOT	BEGINNING: <u>10.3</u> FT/IN OUT
BEGINNING: <u>74662.3</u> HRS	BEGINNING: <u>73658.8</u> HRS	TOTAL: <u>251.3</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>11.00</u>
AVG. STEAM FLOW: <u>61.2</u> KLB/HR	AVG. STEAM FLOW: <u>63.8</u> KLB/HR	ENDING: <u>2727800</u> JEM TOT	
APPROX REF PROC: <u>157.3</u> TONS	APPROX REF PROC: <u>184.9</u> TONS	BEGINNING: <u>2727800</u> JEM TOT	CARBON USAGE:
REFUSE PROCESSED: <u>244.8</u> TONS	REFUSE PROCESSED: <u>255.2</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #1: <u>552</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	USAGE UNIT #2: <u>552</u> LBS
TOTAL STEAM FLOW: <u>3000.4</u> KLB	GROSS REFUSE REC: <u>260.47</u> TONS	IN PLANT USE: <u>36.7</u> MWH	DAILY TOTAL: <u>1104</u> LBS
TOTAL REFUSE PR. <u>348.3</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>105.4</u>	CARBON INVENTORY:
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		ENDING: <u>19</u> FT. OUT <u>95</u> IN OUT
ENDING: <u>421832000</u> GAL	TOTAL REFUSE REC: <u>260.47</u> TONS	MEDICAL WASTE:	BEGINNING: <u>20</u> FT. OUT <u>17</u> IN OUT
BEGINNING: <u>421554000</u> GAL	EST PIT INVENTORY: <u>1,867.0</u> TONS	PROCESSED: <u>6.15</u> TONS	RECEIVED: <u>0.00</u> TONS
TOTAL USED: <u>278000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.77</u> %	EOM OUT: <u>26.92</u>
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>95.1</u> %	UNIT 2 % MCR: <u>99.0</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.4</u>	GROSS KW/TON PR. <u>826.8</u>	
NET KWH/TON PR. <u>721.4</u>	LB LIME/TON PR.: <u>6.3</u>	TOT STM TO T/G: <u>3,031.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 9 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1330.9</u> KLB	STEAM PRODUCED: <u>1397.7</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1375.3</u> KLB	FEEDWATER USED: <u>1474.2</u> KLB	ENDING: <u>8586.0</u> WH TOT	BEGINNING: <u>180807</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8576.0</u> WH TOT	ENDING: <u>180828</u> CU FT
BLOWDOWN: <u>44</u> KLB	BLOWDOWN: <u>77</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>21</u> CU FT
BLOWDOWN: <u>3.2</u> %	BLOWDOWN: <u>5.2</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>9990240</u> JEM TOT	ENDING: <u>11.4</u> FT/IN OUT
ENDING: <u>74709.3</u> HRS	ENDING: <u>73706.8</u> HRS	BEGINNING: <u>9765980</u> JEM TOT	BEGINNING: <u>11.0</u> FT/IN OUT
BEGINNING: <u>74685.3</u> HRS	BEGINNING: <u>73682.8</u> HRS	TOTAL: <u>224.3</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>11.33</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.5</u> KLB/HR	AVG. STEAM FLOW: <u>58.2</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>144.1</u> TONS	APPROX REF PROC: <u>142.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>221.8</u> TONS	REFUSE PROCESSED: <u>233.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>63.7</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2728.6</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS	KWH/TON: <u>222.5</u>	ENDING: <u>19</u> FT. OUT <u>63</u> IN OUT
TOTAL REFUSE PR. <u>286.4</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>19</u> FT. OUT <u>95</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
ENDING: <u>422098000</u> GAL	TOTAL REFUSE REC: <u>0.00</u> TONS	MEDICAL WASTE:	EOM OUT: <u>24.25</u>
BEGINNING: <u>421832000</u> GAL	EST PIT INVENTORY: <u>1,342.0</u> TONS	PROCESSED: <u>0.00</u> TONS	
TOTAL USED: <u>266000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>86.1</u> %	UNIT 2 % MCR: <u>90.4</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.5</u>	GROSS KW/TON PR. <u>1005.5</u>	
NET KWH/TON PR. <u>782.9</u>	LB LIME/TON PR.: <u>4.4</u>	TOT STM TO T/G: <u>2,758.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE MAY 10 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1300.1</u> KLB	STEAM PRODUCED: <u>1365.6</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1341.9</u> KLB	FEEDWATER USED: <u>1426.7</u> KLB	ENDING: <u>8596.0</u> WH TOT	BEGINNING: <u>180828</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8586.0</u> WH TOT	ENDING: <u>180834</u> CU FT
BLOWDOWN: <u>42</u> KLB	BLOWDOWN: <u>61</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>6</u> CU FT
BLOWDOWN: <u>3.1</u> %	BLOWDOWN: <u>4.3</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>10209270</u> JEM TOT	ENDING: <u>12.4</u> FT/IN OUT
ENDING: <u>74733.3</u> HRS	ENDING: <u>73730.8</u> HRS	BEGINNING: <u>9990240</u> JEM TOT	BEGINNING: <u>11.4</u> FT/IN OUT
BEGINNING: <u>74709.3</u> HRS	BEGINNING: <u>73706.8</u> HRS	TOTAL: <u>219.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>12.33</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>54.2</u> KLB/HR	AVG. STEAM FLOW: <u>56.9</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>232.0</u> TONS	APPROX REF PROC: <u>227.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>216.7</u> TONS	REFUSE PROCESSED: <u>227.6</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>69.0</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2665.7</u> KLB	GROSS REFUSE REC: <u>673.08</u> TONS	KWH/TON: <u>153.8</u>	ENDING: <u>19</u> FT. OUT <u>21</u> IN OUT
TOTAL REFUSE PR. <u>448.4</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING <u>19</u> FT. OUT <u>63</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
ENDING: <u>422360000</u> GAL	TOTAL REFUSE REC: <u>673.08</u> TONS	MEDICAL WASTE:	EOM OUT: <u>20.75</u>
BEGINNING: <u>422098000</u> GAL	EST PIT INVENTORY: <u>1.634.0</u> TONS	PROCESSED: <u>4.12</u> TONS	
TOTAL USED: <u>262000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.92</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>84.1</u> %	UNIT 2 % MCR: <u>88.4</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.3</u>	GROSS KW/TON PR. <u>642.3</u>	
NET KWH/TON PR. <u>488.5</u>	LB LIME/TON PR.: <u>7.0</u>	TOT STM TO T/G: <u>2,675.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 11 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1352.5</u> KLB	STEAM PRODUCED: <u>1450.5</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1397.1</u> KLB	FEEDWATER USED: <u>1523.7</u> KLB	ENDING: <u>8605.0</u> WH TOT	BEGINNING: <u>180834</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8596.0</u> WH TOT	ENDING: <u>180835</u> CU FT
BLOWDOWN: <u>45</u> KLB	BLOWDOWN: <u>73</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>3.2</u> %	BLOWDOWN: <u>4.8</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>442030</u> JEM TOT	ENDING: <u>9.0</u> FT/IN OUT
ENDING: <u>74757.3</u> HRS	ENDING: <u>73754.8</u> HRS	BEGINNING: <u>209270</u> JEM TOT	BEGINNING: <u>12.4</u> FT/IN OUT
BEGINNING: <u>74733.3</u> HRS	BEGINNING: <u>73730.8</u> HRS	TOTAL: <u>232.8</u> MWH	RECEIVED: <u>25.72</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.00</u>
AVG. STEAM FLOW: <u>56.4</u> KLB/HR	AVG. STEAM FLOW: <u>60.4</u> KLB/HR	ENDING: <u>2727800</u> JEM TOT	
APPROX REF PROC: <u>230.1</u> TONS	APPROX REF PROC: <u>231.0</u> TONS	BEGINNING: <u>2727800</u> JEM TOT	CARBON USAGE:
REFUSE PROCESSED: <u>225.4</u> TONS	REFUSE PROCESSED: <u>241.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #1: <u>552</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	USAGE UNIT #2: <u>552</u> LBS
		IN PLANT USE: <u>26.4</u> MWH	DAILY TOTAL: <u>1104</u> LBS
TOTAL STEAM FLOW: <u>2803.0</u> KLB	GROSS REFUSE REC: <u>629.01</u> TONS	KWH/TON: <u>56.6</u>	CARBON INVENTORY:
TOTAL REFUSE PR. <u>466.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS		ENDING: <u>18</u> FT. OUT <u>46</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS		BEGINNING: <u>19</u> FT. OUT <u>21</u> IN OUT
	TOTAL REFUSE REC: <u>629.01</u> TONS		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	EST PIT INVENTORY: <u>1,867.0</u> TONS	MEDICAL WASTE :	EOM OUT: <u>21.83</u>
ENDING: <u>422630000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>5.63</u> TONS	
BEGINNING: <u>422360000</u> GAL		% OF REFUSE PROC: <u>1.21</u> %	
TOTAL USED: <u>270000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>87.5</u> %	UNIT 2 % MCR: <u>93.8</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.8</u>	GROSS KW/TON PR. <u>555.4</u>	
NET KWH/TON PR. <u>498.7</u>	LB LIME/TON PR.: <u>87.3</u>	TOT STM TO T/G: <u>2,826.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 12 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1424.6</u> KLB	STEAM PRODUCED: <u>1450.6</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1471.9</u> KLB	FEEDWATER USED: <u>1532.5</u> KLB	ENDING: <u>8615.0</u> WH TOT	BEGINNING: <u>180835</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8605.0</u> WH TOT	ENDING: <u>180836</u> CU FT
BLOWDOWN: <u>47</u> KLB	BLOWDOWN: <u>82</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>3.2</u> %	BLOWDOWN: <u>5.3</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>684560</u> JEM TOT	ENDING: <u>10.0</u> FT/IN OUT
ENDING: <u>74781.3</u> HRS	ENDING: <u>73778.8</u> HRS	BEGINNING: <u>442030</u> JEM TOT	BEGINNING: <u>9.0</u> FT/IN OUT
BEGINNING: <u>74757.3</u> HRS	BEGINNING: <u>73754.8</u> HRS	TOTAL: <u>242.5</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>10.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.4</u> KLB/HR	AVG. STEAM FLOW: <u>60.4</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>244.0</u> TONS	APPROX REF PROC: <u>232.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>237.4</u> TONS	REFUSE PROCESSED: <u>241.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>45.5</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2875.2</u> KLB	GROSS REFUSE REC: <u>610.83</u> TONS	KWH/TON: <u>92.8</u>	ENDING: <u>18</u> FT. OUT <u>78</u> IN OUT
TOTAL REFUSE PR. <u>490.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>18</u> FT. OUT <u>46</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
ENDING: <u>422907000</u> GAL	TOTAL REFUSE REC: <u>610.83</u> TONS	MEDICAL WASTE:	EOM OUT: <u>24.50</u>
BEGINNING: <u>422630000</u> GAL	EST PIT INVENTORY: <u>1,284.0</u> TONS	PROCESSED: <u>13.98</u> TONS	
TOTAL USED: <u>277000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.85</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>92.2</u> %	UNIT 2 % MCR: <u>93.9</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.0</u>	GROSS KW/TON PR. <u>587.8</u>	
NET KWH/TON PR. <u>495.0</u>	LB LIME/TON PR.: <u>6.4</u>	TOT STM TO T/G: <u>2,918.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 13, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1383.1</u> KLB	STEAM PRODUCED: <u>1392.3</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1430.0</u> KLB	FEEDWATER USED: <u>1451.0</u> KLB	ENDING: <u>8625.0</u> WH TOT	BEGINNING: <u>180836</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8615.0</u> WH TOT	ENDING: <u>180836</u> CU FT
BLOWDOWN: <u>47</u> KLB	BLOWDOWN: <u>59</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>4.0</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>913150</u> JEM TOT	ENDING: <u>11.3</u> FT/IN OUT
ENDING: <u>74805.3</u> HRS	ENDING: <u>73802.6</u> HRS	BEGINNING: <u>684560</u> JEM TOT	BEGINNING: <u>10.0</u> FT/IN OUT
BEGINNING: <u>74781.3</u> HRS	BEGINNING: <u>73778.8</u> HRS	TOTAL: <u>228.6</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.8</u> HRS	UTILITY IN:	EOM OUT: <u>11.21</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>57.6</u> KLB/HR	AVG. STEAM FLOW: <u>58.0</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>222.0</u> TONS	APPROX REF PROC: <u>231.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>230.5</u> TONS	REFUSE PROCESSED: <u>232.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>59.4</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>129.1</u>	ENDING: <u>17</u> FT. OUT <u>97</u> IN OUT
TOTAL STEAM FLOW: <u>2775.4</u> KLB	GROSS REFUSE REC: <u>425.28</u> TONS		BEGINNING: <u>18</u> FT. OUT <u>78</u> IN OUT
TOTAL REFUSE PR. <u>460.3</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS		EOM OUT: <u>25.08</u>
	TOTAL REFUSE REC: <u>425.28</u> TONS		
WELL WATER USE:	EST PIT INVENTORY: <u>1,575.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>423162000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>7.28</u> TONS	
BEGINNING: <u>422907000</u> GAL		% OF REFUSE PROC: <u>1.58</u> %	
TOTAL USED: <u>255000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>89.5</u> %	UNIT 2 % MCR: <u>90.1</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.6</u>	GROSS KW/TON PR. <u>625.7</u>	
NET KWH/TON PR. <u>496.6</u>	LB LIME/TON PR.: <u>8.5</u>	TOT STM TO T/G: <u>2,784.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 14, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1260.1</u> KLB	STEAM PRODUCED: <u>1311.7</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1300.3</u> KLB	FEEDWATER USED: <u>1375.8</u> KLB	ENDING: <u>8633.0</u> WH TOT	BEGINNING: <u>180836</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8625.0</u> WH TOT	ENDING: <u>180876</u> CU FT
BLOWDOWN: <u>40</u> KLB	BLOWDOWN: <u>64</u> KLB	TOTAL: <u>230.4</u> MWH	TOTAL USED: <u>40</u> CU FT
BLOWDOWN: <u>3.1</u> %	BLOWDOWN: <u>4.7</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1119340</u> JEM TOT	ENDING: <u>11.7</u> FT/IN OUT
ENDING: <u>74829.3</u> HRS	ENDING: <u>73826.1</u> HRS	BEGINNING: <u>913150</u> JEM TOT	BEGINNING: <u>11.3</u> FT/IN OUT
BEGINNING: <u>74805.3</u> HRS	BEGINNING: <u>73802.6</u> HRS	TOTAL: <u>206.2</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.5</u> HRS	UTILITY IN:	EOM OUT: <u>11.55</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>52.5</u> KLB/HR	AVG. STEAM FLOW: <u>54.7</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>161.0</u> TONS	APPROX REF PROC: <u>163.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>210.0</u> TONS	REFUSE PROCESSED: <u>218.6</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>24.2</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>74.7</u>	ENDING: <u>18</u> FT. OUT <u>9</u> IN OUT
TOTAL STEAM FLOW: <u>2571.8</u> KLB	GROSS REFUSE REC: <u>79.71</u> TONS		BEGINNING: <u>17</u> FT. OUT <u>97</u> IN OUT
TOTAL REFUSE PR. <u>324.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS		EOM OUT: <u>18.75</u>
	TOTAL REFUSE REC: <u>79.71</u> TONS		
WELL WATER USE:	EST PIT INVENTORY: <u>1,050.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>423406000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>423162000</u> GAL		% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>244000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>81.5</u> %	UNIT 2 % MCR: <u>84.9</u> %	TG % MCR: <u>61.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>11.2</u>	GROSS KW/TON PR. <u>711.1</u>	
NET KWH/TON PR. <u>636.4</u>	LB LIME/TON PR.: <u>3.5</u>	TOT STM TO T/G: <u>2,555.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 15, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1279.6</u> KLB	STEAM PRODUCED: <u>1328.2</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1322.7</u> KLB	FEEDWATER USED: <u>1383.4</u> KLB	ENDING: <u>8643.0</u> WH TOT	BEGINNING: <u>180876</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8633.0</u> WH TOT	ENDING: <u>180885</u> CU FT
BLOWDOWN: <u>43</u> KLB	BLOWDOWN: <u>55</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>9</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>4.0</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1332190</u> JEM TOT	ENDING: <u>12.0</u> FT/IN OUT
ENDING: <u>74853.3</u> HRS	ENDING: <u>73850.1</u> HRS	BEGINNING: <u>1119340</u> JEM TOT	BEGINNING: <u>11.7</u> FT/IN OUT
BEGINNING: <u>74829.3</u> HRS	BEGINNING: <u>73826.1</u> HRS	TOTAL: <u>212.9</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>12.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>53.3</u> KLB/HR	AVG. STEAM FLOW: <u>55.3</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>201.0</u> TONS	APPROX REF PROC: <u>202.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>213.3</u> TONS	REFUSE PROCESSED: <u>221.4</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>75.2</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2607.7</u> KLB	GROSS REFUSE REC: <u>398.63</u> TONS	KWH/TON: <u>176.4</u>	ENDING: <u>17</u> FT. OUT <u>35</u> IN OUT
TOTAL REFUSE PR. <u>426.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING <u>18</u> FT. OUT <u>9</u> IN OUT
	FERROUS HAULED: <u>32.63</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>366.00</u> TONS		EOM OUT: <u>19.92</u>
WELL WATER USE:	EST PIT INVENTORY: <u>1,458.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>423670000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>23.00</u> TONS	
BEGINNING: <u>423406000</u> GAL		% OF REFUSE PROC: <u>5.40</u> %	
TOTAL USED: <u>264000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>82.8</u> %	UNIT 2 % MCR: <u>85.9</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.1</u>	GROSS KW/TON PR. <u>676.1</u>	
NET KWH/TON PR. <u>499.6</u>	LB LIME/TON PR.: <u>2.2</u>	TOT STM TO T/G: <u>2,619.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 16, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1324.1</u> KLB	STEAM PRODUCED: <u>1362.9</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1368.3</u> KLB	FEEDWATER USED: <u>1428.3</u> KLB	ENDING: <u>8652.0</u> WH TOT	BEGINNING: <u>180885</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8643.0</u> WH TOT	ENDING: <u>180936</u> CU FT
BLOWDOWN: <u>44</u> KLB	BLOWDOWN: <u>65</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>51</u> CU FT
BLOWDOWN: <u>3.2</u> %	BLOWDOWN: <u>4.6</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1554340</u> JEM TOT	ENDING: <u>12.7</u> FT/IN OUT
ENDING: <u>74877.3</u> HRS	ENDING: <u>73873.8</u> HRS	BEGINNING: <u>1332190</u> JEM TOT	BEGINNING: <u>12.0</u> FT/IN OUT
BEGINNING: <u>74853.3</u> HRS	BEGINNING: <u>73850.1</u> HRS	TOTAL: <u>222.2</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.7</u> HRS	UTILITY IN:	EOM OUT: <u>12.55</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.2</u> KLB/HR	AVG. STEAM FLOW: <u>56.8</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>279.8</u> TONS	APPROX REF PROC: <u>271.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>220.7</u> TONS	REFUSE PROCESSED: <u>227.2</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>37.0</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2687.0</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS	KWH/TON: <u>82.7</u>	ENDING: <u>16</u> FT. OUT <u>69</u> IN OUT
TOTAL REFUSE PR. <u>447.8</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>17</u> FT. OUT <u>35</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
ENDING: <u>423932000</u> GAL	TOTAL REFUSE REC: <u>0.00</u> TONS	MEDICAL WASTE:	EOM OUT: <u>21.75</u>
BEGINNING: <u>423670000</u> GAL	EST PIT INVENTORY: <u>817.0</u> TONS	PROCESSED: <u>0.00</u> TONS	
TOTAL USED: <u>262000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.7</u> %	UNIT 2 % MCR: <u>88.2</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.4</u>	GROSS KW/TON PR. <u>578.8</u>	
NET KWH/TON PR. <u>496.1</u>	LB LIME/TON PR.: <u>4.6</u>	TOT STM TO T/G: <u>2,717.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 17, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1321.0</u> KLB	STEAM PRODUCED: <u>1362.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1362.0</u> KLB	FEEDWATER USED: <u>1438.0</u> KLB	ENDING: <u>8661.0</u> WH TOT	BEGINNING: <u>180936</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8652.0</u> WH TOT	ENDING: <u>181177</u> CU FT
BLOWDOWN: <u>41</u> KLB	BLOWDOWN: <u>76</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>241</u> CU FT
BLOWDOWN: <u>3.0</u> %	BLOWDOWN: <u>5.3</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1774700</u> JEM TOT	ENDING: <u>13.5</u> FT/IN OUT
ENDING: <u>74901.3</u> HRS	ENDING: <u>73897.8</u> HRS	BEGINNING: <u>1554340</u> JEM TOT	BEGINNING: <u>12.7</u> FT/IN OUT
BEGINNING: <u>74877.3</u> HRS	BEGINNING: <u>73873.8</u> HRS	TOTAL: <u>220.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>13.42</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.0</u> KLB/HR	AVG. STEAM FLOW: <u>56.8</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>238.0</u> TONS	APPROX REF PROC: <u>255.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>220.2</u> TONS	REFUSE PROCESSED: <u>227.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>38.8</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>85.9</u>	ENDING: <u>16</u> FT. OUT <u>52</u> IN OUT
TOTAL STEAM FLOW: <u>2683.0</u> KLB	GROSS REFUSE REC: <u>713.68</u> TONS		BEGINNING: <u>16</u> FT. OUT <u>69</u> IN OUT
TOTAL REFUSE PR. <u>452.4</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS		EOM OUT: <u>20.33</u>
	TOTAL REFUSE REC: <u>713.68</u> TONS		
WELL WATER USE:	EST PIT INVENTORY: <u>1,225.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>424205000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>5.21</u> TONS	
BEGINNING: <u>423932000</u> GAL		% OF REFUSE PROC: <u>1.15</u> %	
TOTAL USED: <u>273000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.5</u> %	UNIT 2 % MCR: <u>88.1</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.4</u>	GROSS KW/TON PR. <u>573.0</u>	
NET KWH/TON PR. <u>487.1</u>	LB LIME/TON PR.: <u>5.6</u>	TOT STM TO T/G: <u>2,630.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 18, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1397.0</u> KLB	STEAM PRODUCED: <u>1407.5</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1449.5</u> KLB	FEEDWATER USED: <u>1473.5</u> KLB	ENDING: <u>8671.0</u> WH TOT	BEGINNING: <u>181177</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8661.0</u> WH TOT	ENDING: <u>181184</u> CU FT
BLOWDOWN: <u>47</u> KLB	BLOWDOWN: <u>66</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>7</u> CU FT
BLOWDOWN: <u>3.2</u> %	BLOWDOWN: <u>4.5</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2005760</u> JEM TOT	ENDING: <u>10.5</u> FT/M OUT
ENDING: <u>74925.3</u> HRS	ENDING: <u>73921.8</u> HRS	BEGINNING: <u>1774700</u> JEM TOT	BEGINNING: <u>13.5</u> FT/M OUT
BEGINNING: <u>74901.3</u> HRS	BEGINNING: <u>73897.8</u> HRS	TOTAL: <u>231.1</u> MWH	RECEIVED: <u>24.27</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>10.42</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>58.2</u> KLB/HR	AVG. STEAM FLOW: <u>58.6</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>206.3</u> TONS	APPROX REF PROC: <u>214.6</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>232.8</u> TONS	REFUSE PROCESSED: <u>234.6</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>56.9</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2804.5</u> KLB	GROSS REFUSE REC: <u>714.53</u> TONS	KWH/TON: <u>132.4</u>	ENDING: <u>16</u> FT. OUT <u>30</u> IN OUT
TOTAL REFUSE PR. <u>430.1</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>16</u> FT. OUT <u>52</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>714.53</u> TONS		EOM OUT: <u>18.50</u>
WELL WATER USE:	EST PIT INVENTORY: <u>1,576.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>424468000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>9.22</u> TONS	
BEGINNING: <u>424205000</u> GAL		% OF REFUSE PROC: <u>2.14</u> %	
TOTAL USED: <u>263000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>90.4</u> %	UNIT 2 % MCR: <u>91.1</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.7</u>	GROSS KW/TON PR. <u>669.6</u>	
NET KWH/TON PR. <u>537.2</u>	LB LIME/TON PR.: <u>91.0</u>	TOT STM TO T/G: <u>2,820.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 19, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1389.0</u> KLB	STEAM PRODUCED: <u>1384.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1433.5</u> KLB	FEEDWATER USED: <u>1439.0</u> KLB	ENDING: <u>8680.0</u> WH TOT	BEGINNING: <u>181184</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8671.0</u> WH TOT	ENDING: <u>181184</u> CU FT
BLOWDOWN: <u>45</u> KLB	BLOWDOWN: <u>55</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN %: <u>3.1</u> %	BLOWDOWN %: <u>3.8</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2235500</u> JEM TOT	ENDING: <u>10.9</u> FT/IN OUT
ENDING: <u>74949.3</u> HRS	ENDING: <u>73945.8</u> HRS	BEGINNING: <u>2005760</u> JEM TOT	BEGINNING: <u>10.5</u> FT/IN OUT
BEGINNING: <u>74925.3</u> HRS	BEGINNING: <u>73921.8</u> HRS	TOTAL: <u>229.7</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>10.75</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>57.9</u> KLB/HR	AVG. STEAM FLOW: <u>57.7</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>216.5</u> TONS	APPROX REF PROC: <u>201.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>231.5</u> TONS	REFUSE PROCESSED: <u>230.7</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>29.5</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2773.0</u> KLB	GROSS REFUSE REC: <u>612.78</u> TONS	KWH/TON: <u>69.9</u>	ENDING: <u>16</u> FT. OUT <u>25</u> IN OUT
TOTAL REFUSE PR. <u>421.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>16</u> FT. OUT <u>30</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
ENDING: <u>424728000</u> GAL	TOTAL REFUSE REC: <u>612.78</u> TONS	MEDICAL WASTE:	EOM OUT: <u>18.08</u>
BEGINNING: <u>424468000</u> GAL	EST PIT INVENTORY: <u>1,828.0</u> TONS	PROCESSED: <u>4.06</u> TONS	
TOTAL USED: <u>260000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.96</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>89.9</u> %	UNIT 2 % MCR: <u>89.5</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.7</u>	GROSS KW/TON PR. <u>614.8</u>	
NET KWH/TON PR. <u>545.0</u>	LB LIME/TON PR.: <u>3.0</u>	TOT STM TO T/G: <u>2,790.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE May 20, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1403.0</u> KLB	STEAM PRODUCED: <u>1398.8</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1448.3</u> KLB	FEEDWATER USED: <u>1461.4</u> KLB	ENDING: <u>8690.0</u> WH TOT	BEGINNING: <u>181184</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8660.0</u> WH TOT	ENDING: <u>181185</u> CU FT
BLOWDOWN: <u>45</u> KLB	BLOWDOWN: <u>63</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>3.1</u> %	BLOWDOWN: <u>4.3</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2466890</u> JEM TOT	ENDING: <u>11.6</u> FT/IN OUT
ENDING: <u>74973.3</u> HRS	ENDING: <u>73969.8</u> HRS	BEGINNING: <u>2235500</u> JEM TOT	BEGINNING: <u>10.9</u> FT/IN OUT
BEGINNING: <u>74949.3</u> HRS	BEGINNING: <u>73945.8</u> HRS	TOTAL: <u>231.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>11.50</u>
AVG. STEAM FLOW: <u>58.5</u> KLB/HR	AVG. STEAM FLOW: <u>58.3</u> KLB/HR	ENDING: <u>2727800</u> JEM TOT	
APPROX REF PROC: <u>244.0</u> TONS	APPROX REF PROC: <u>217.0</u> TONS	BEGINNING: <u>2727800</u> JEM TOT	CARBON USAGE:
REFUSE PROCESSED: <u>233.8</u> TONS	REFUSE PROCESSED: <u>233.1</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #1: <u>552</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	USAGE UNIT #2: <u>552</u> LBS
TOTAL STEAM FLOW: <u>2801.8</u> KLB	GROSS REFUSE REC: <u>563.78</u> TONS	IN PLANT USE: <u>56.6</u> MWH	DAILY TOTAL: <u>1104</u> LBS
TOTAL REFUSE PR. <u>479.6</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>118.0</u>	CARBON INVENTORY:
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		ENDING: <u>15</u> FT. OUT <u>58</u> IN OUT
ENDING: <u>424989000</u> GAL	TOTAL REFUSE REC: <u>563.78</u> TONS	MEDICAL WASTE :	BEGINNING: <u>16</u> FT. OUT <u>25</u> IN OUT
BEGINNING: <u>424728000</u> GAL	EST PIT INVENTORY: <u>1,575.0</u> TONS	PROCESSED: <u>18.56</u> TONS	RECEIVED: <u>0.00</u> TONS
TOTAL USED: <u>261000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>3.87</u> %	EOM OUT: <u>19.83</u>
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>90.8</u> %	UNIT 2 % MCR: <u>90.5</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.7</u>	GROSS KW/TON PR. <u>600.6</u>	
NET KWH/TON PR. <u>482.5</u>	LB LIME/TON PR.: <u>4.6</u>	TOT STM TO T/G: <u>2,807.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 21, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1393.2</u> KLB	STEAM PRODUCED: <u>1399.1</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1438.2</u> KLB	FEEDWATER USED: <u>1474.3</u> KLB	ENDING: <u>8700.0</u> WH TOT	BEGINNING: <u>181185</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8690.0</u> WH TOT	ENDING: <u>181185</u> CU FT
BLOWDOWN: <u>45</u> KLB	BLOWDOWN: <u>75</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.1</u> %	BLOWDOWN: <u>5.1</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2698570</u> JEM TOT	ENDING: <u>7.4</u> FT/IN OUT
ENDING: <u>74997.3</u> HRS	ENDING: <u>73993.8</u> HRS	BEGINNING: <u>2466890</u> JEM TOT	BEGINNING: <u>11.6</u> FT/IN OUT
BEGINNING: <u>74973.3</u> HRS	BEGINNING: <u>73969.8</u> HRS	TOTAL: <u>231.7</u> MWH	RECEIVED: <u>24.80</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>7.33</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>58.0</u> KLB/HR	AVG. STEAM FLOW: <u>58.3</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>214.0</u> TONS	APPROX REF PROC: <u>204.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>232.2</u> TONS	REFUSE PROCESSED: <u>233.2</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>56.3</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2792.3</u> KLB	GROSS REFUSE REC: <u>588.73</u> TONS	KWH/TON: <u>130.1</u>	ENDING: <u>15</u> FT. OUT <u>17</u> IN OUT
TOTAL REFUSE PR. <u>433.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>58</u> IN OUT
	FERROUS HAULED: <u>35.64</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>553.09</u> TONS		EOM OUT: <u>16.42</u>
WELL WATER USE:	EST PIT INVENTORY: <u>1,633.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>425263000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>14.98</u> TONS	
BEGINNING: <u>424889000</u> GAL		% OF REFUSE PROC: <u>3.46</u> %	
TOTAL USED: <u>274000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>90.1</u> %	UNIT 2 % MCR: <u>90.5</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.7</u>	GROSS KW/TON PR. <u>665.2</u>	
NET KWH/TON PR. <u>535.1</u>	LB LIME/TON PR.: <u>84.1</u>	TOT STM TO T/G: <u>2,812.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE. INC.
DAILY PRODUCTION REPORT
DATE May 22, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1406.3</u> KLB	STEAM PRODUCED: <u>718.6</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1450.0</u> KLB	FEEDWATER USED: <u>777.4</u> KLB	ENDING: <u>8707.0</u> WH TOT	BEGINNING: <u>181185</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8700.0</u> WH TOT	ENDING: <u>181250</u> CU FT
BLOWDOWN: <u>44</u> KLB	BLOWDOWN: <u>59</u> KLB	TOTAL: <u>201.6</u> MWH	TOTAL USED: <u>65</u> CU FT
BLOWDOWN: <u>3.0</u> %	BLOWDOWN: <u>7.6</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2864000</u> JEM TOT	ENDING: <u>7.9</u> FT/IN OUT
ENDING: <u>75021.3</u> HRS	ENDING: <u>74005.9</u> HRS	BEGINNING: <u>2698570</u> JEM TOT	BEGINNING: <u>7.4</u> FT/IN OUT
BEGINNING: <u>74997.3</u> HRS	BEGINNING: <u>73993.8</u> HRS	TOTAL: <u>165.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>12.1</u> HRS	UTILITY IN:	EOM OUT: <u>7.75</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>12.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>58.6</u> KLB/HR	AVG. STEAM FLOW: <u>59.9</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>196.2</u> TONS	APPROX REF PROC: <u>84.5</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>276</u> LBS
REFUSE PROCESSED: <u>234.4</u> TONS	REFUSE PROCESSED: <u>119.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>828</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>36.2</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2124.9</u> KLB	GROSS REFUSE REC: <u>268.85</u> TONS	KWH/TON: <u>123.7</u>	ENDING: <u>15</u> FT. OUT <u>7</u> IN OUT
TOTAL REFUSE PR. <u>292.4</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>17</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>268.85</u> TONS		EOM OUT: <u>15.58</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,031.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>425481000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>11.67</u> TONS	
BEGINNING: <u>425263000</u> GAL		% OF REFUSE PROC: <u>3.99</u> %	
TOTAL USED: <u>218000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>50.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>91.0</u> %	UNIT 2 % MCR: <u>46.5</u> %	TG % MCR: <u>53.5</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.5</u>	GROSS KW/TON PR. <u>669.5</u>	
NET KWH/TON PR. <u>565.8</u>	LB LIME/TON PR.: <u>5.4</u>	TOT STM TO T/G: <u>2,075.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#2 blr off line @ 1200 for discharger repairs.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 23, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1431.2</u> KLB	STEAM PRODUCED: <u>629.8</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1475.3</u> KLB	FEEDWATER USED: <u>686.3</u> KLB	ENDING: <u>8714.0</u> WH TOT	BEGINNING: <u>181250</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8707.0</u> WH TOT	ENDING: <u>181578</u> CU FT
BLOWDOWN: <u>44</u> KLB	BLOWDOWN: <u>57</u> KLB	TOTAL: <u>201.6</u> MWH	TOTAL USED: <u>328</u> CU FT
BLOWDOWN: <u>3.0</u> %	BLOWDOWN: <u>8.2</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3012240</u> JEM TOT	ENDING: <u>8.4</u> FT/IN OUT
ENDING: <u>75045.3</u> HRS	ENDING: <u>74021.2</u> HRS	BEGINNING: <u>2864000</u> JEM TOT	BEGINNING: <u>7.9</u> FT/IN OUT
BEGINNING: <u>75021.3</u> HRS	BEGINNING: <u>74005.9</u> HRS	TOTAL: <u>148.2</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>15.3</u> HRS	UTILITY IN:	EOM OUT: <u>8.33</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>13.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.6</u> KLB/HR	AVG. STEAM FLOW: <u>48.4</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>218.4</u> TONS	APPROX REF PROC: <u>90.4</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>299</u> LBS
REFUSE PROCESSED: <u>238.5</u> TONS	REFUSE PROCESSED: <u>105.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>851</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>53.4</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>169.3</u>	ENDING: <u>15</u> FT. OUT <u>0</u> IN OUT
TOTAL STEAM FLOW: <u>2061.0</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>7</u> IN OUT
TOTAL REFUSE PR. <u>315.2</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS		EOM OUT: <u>15.00</u>
	TOTAL REFUSE REC: <u>0.00</u> TONS		
WELL WATER USE:	EST PIT INVENTORY: <u>1,517.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>425694000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>6.45</u> TONS	
BEGINNING: <u>425481000</u> GAL		% OF REFUSE PROC: <u>2.05</u> %	
TOTAL USED: <u>213000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>54.2</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>92.6</u> %	UNIT 2 % MCR: <u>40.7</u> %	TG % MCR: <u>53.5</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>639.6</u>	
NET KWH/TON PR. <u>470.3</u>	LB LIME/TON PR.: <u>5.0</u>	TOT STM TO T/G: <u>1,854.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#2 blr off line for discharger repair, burner in #2 @ 0912.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
 DATE May 24, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1329.0</u> KLB	STEAM PRODUCED: <u>1381.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1372.0</u> KLB	FEEDWATER USED: <u>1438.0</u> KLB	ENDING: <u>8723.0</u> WH TOT	BEGINNING: <u>181578</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8714.0</u> WH TOT	ENDING: <u>181578</u> CU FT
BLOWDOWN: <u>43</u> KLB	BLOWDOWN: <u>57</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.1</u> %	BLOWDOWN: <u>4.0</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3231860</u> JEM TOT	ENDING: <u>9.2</u> FT/IN OUT
ENDING: <u>75069.3</u> HRS	ENDING: <u>74045.2</u> HRS	BEGINNING: <u>3012240</u> JEM TOT	BEGINNING: <u>8.4</u> FT/IN OUT
BEGINNING: <u>75045.3</u> HRS	BEGINNING: <u>74021.2</u> HRS	TOTAL: <u>219.7</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.17</u>
AVG. STEAM FLOW: <u>55.4</u> KLB/HR	AVG. STEAM FLOW: <u>57.5</u> KLB/HR	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>228.2</u> TONS	APPROX REF PROC: <u>201.6</u> TONS	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
REFUSE PROCESSED: <u>221.5</u> TONS	REFUSE PROCESSED: <u>230.2</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
TOTAL STEAM FLOW: <u>2710.0</u> KLB	GROSS REFUSE REC: <u>662.01</u> TONS	IN PLANT USE: <u>39.5</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>444.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>88.9</u>	ENDING: <u>14</u> FT. OUT <u>53</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>0</u> IN OUT
ENDING: <u>425955000</u> GAL	TOTAL REFUSE REC: <u>662.01</u> TONS	MEDICAL WASTE:	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>425694000</u> GAL	EST PIT INVENTORY: <u>1,712.0</u> TONS	PROCESSED: <u>14.18</u> TONS	EOM OUT: <u>18.42</u>
TOTAL USED: <u>261000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>3.19</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>86.0</u> %	UNIT 2 % MCR: <u>89.4</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.5</u>	GROSS KW/TON PR. <u>583.8</u>	
NET KWH/TON PR. <u>494.9</u>	LB LIME/TON PR.: <u>5.7</u>	TOT STM TO T/G: <u>2,698.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 25, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1390.0</u> KLB	STEAM PRODUCED: <u>1408.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1435.0</u> KLB	FEEDWATER USED: <u>1490.0</u> KLB	ENDING: <u>8732.0</u> WH TOT	BEGINNING: <u>181578</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8723.0</u> WH TOT	ENDING: <u>181578</u> CU FT
BLOWDOWN: <u>45</u> KLB	BLOWDOWN: <u>82</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>3.1</u> %	BLOWDOWN: <u>5.5</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3462350</u> JEM TOT	ENDING: <u>10.3</u> FT/IN OUT
ENDING: <u>75093.3</u> HRS	ENDING: <u>74069.0</u> HRS	BEGINNING: <u>3231960</u> JEM TOT	BEGINNING: <u>9.2</u> FT/IN OUT
BEGINNING: <u>75069.3</u> HRS	BEGINNING: <u>74045.2</u> HRS	TOTAL: <u>230.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.8</u> HRS	UTILITY IN:	EOM OUT: <u>10.25</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>57.9</u> KLB/HR	AVG. STEAM FLOW: <u>58.7</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>168.3</u> TONS	APPROX REF PROC: <u>170.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>231.7</u> TONS	REFUSE PROCESSED: <u>234.7</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>28.8</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2798.0</u> KLB	GROSS REFUSE REC: <u>804.75</u> TONS	KWH/TON: <u>85.1</u>	ENDING: <u>13</u> FT. OUT <u>87</u> IN OUT
TOTAL REFUSE PR. <u>338.6</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>14</u> FT. OUT <u>53</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>804.75</u> TONS		EOM OUT: <u>21.08</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,120.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>426219000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>425955000</u> GAL		% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>264000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>89.9</u> %	UNIT 2 % MCR: <u>91.1</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.8</u>	GROSS KW/TON PR. <u>765.5</u>	
NET KWH/TON PR. <u>680.4</u>	LB LIME/TON PR.: <u>10.2</u>	TOT STM TO T/G: <u>2,821.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 26, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1388.0</u> KLB	STEAM PRODUCED: <u>1443.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1435.0</u> KLB	FEEDWATER USED: <u>1529.0</u> KLB	ENDING: <u>8742.0</u> WH TOT	BEGINNING: <u>181579</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8732.0</u> WH TOT	ENDING: <u>181579</u> CU FT
BLOWDOWN: <u>47</u> KLB	BLOWDOWN: <u>86</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>5.6</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3695150</u> JEM TOT	ENDING: <u>6.5</u> FT/IN OUT
ENDING: <u>75117.3</u> HRS	ENDING: <u>74093.0</u> HRS	BEGINNING: <u>3462350</u> JEM TOT	BEGINNING: <u>10.3</u> FT/IN OUT
BEGINNING: <u>75093.3</u> HRS	BEGINNING: <u>74069.0</u> HRS	TOTAL: <u>232.8</u> MWH	RECEIVED: <u>24.60</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>6.42</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>57.8</u> KLB/HR	AVG. STEAM FLOW: <u>80.1</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>106.9</u> TONS	APPROX REF PROC: <u>99.5</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>231.3</u> TONS	REFUSE PROCESSED: <u>240.5</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>55.2</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2831.0</u> KLB	GROSS REFUSE REC: <u>534.45</u> TONS	KWH/TON: <u>257.8</u>	ENDING: <u>13</u> FT. OUT <u>63</u> IN OUT
TOTAL REFUSE PR. <u>214.1</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>13</u> FT. OUT <u>97</u> IN OUT
	FERROUS HAULED: <u>18.93</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>515.52</u> TONS		EOM OUT: <u>18.25</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,140.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>426523000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>7.77</u> TONS	
BEGINNING: <u>426219000</u> GAL		% OF REFUSE PROC: <u>3.63</u> %	
TOTAL USED: <u>304000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>89.8</u> %	UNIT 2 % MCR: <u>93.4</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.8</u>	GROSS KW/TON PR. <u>1345.0</u>	
NET KWH/TON PR. <u>1087.2</u>	LB LIME/TON PR.: <u>174.1</u>	TOT STM TO T/G: <u>2,849.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 27, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1453.0</u> KLB	STEAM PRODUCED: <u>1467.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1500.0</u> KLB	FEEDWATER USED: <u>1552.0</u> KLB	ENDING: <u>8752.0</u> WH TOT	BEGINNING: <u>181579</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8742.0</u> WH TOT	ENDING: <u>181589</u> CU FT
BLOWDOWN: <u>47</u> KLB	BLOWDOWN: <u>85</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>10</u> CU FT
BLOWDOWN : <u>3.1</u> %	BLOWDOWN : <u>5.5</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3937650</u> JEM TOT	ENDING: <u>7.1</u> FT/IN OUT
ENDING: <u>75141.3</u> HRS	ENDING: <u>74117.0</u> HRS	BEGINNING: <u>3895150</u> JEM TOT	BEGINNING: <u>6.5</u> FT/IN OUT
BEGINNING: <u>75117.3</u> HRS	BEGINNING: <u>74093.0</u> HRS	TOTAL: <u>242.5</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>7.08</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>60.5</u> KLB/HR	AVG. STEAM FLOW: <u>61.1</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>164.0</u> TONS	APPROX REF PROC: <u>183.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>242.2</u> TONS	REFUSE PROCESSED: <u>244.5</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>45.5</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2920.0</u> KLB	GROSS REFUSE REC: <u>552.32</u> TONS	KWH/TON: <u>127.5</u>	ENDING: <u>13</u> FT. OUT <u>43</u> IN OUT
TOTAL REFUSE PR. <u>356.8</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>13</u> FT. OUT <u>63</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>552.32</u> TONS		EOM OUT: <u>16.58</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,275.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>426857000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>9.81</u> TONS	
BEGINNING: <u>426523000</u> GAL		% OF REFUSE PROC: <u>2.75</u> %	
TOTAL USED: <u>334000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>94.0</u> %	UNIT 2 % MCR: <u>94.9</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.1</u>	GROSS KW/TON PR. <u>807.2</u>	
NET KWH/TON PR. <u>679.6</u>	LB LIME/TON PR.: <u>5.3</u>	TOT STM TO T/G: <u>2,956.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 28 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1424.1</u> KLB	STEAM PRODUCED: <u>1464.3</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1471.0</u> KLB	FEEDWATER USED: <u>1494.3</u> KLB	ENDING: <u>8761.0</u> WH TOT	BEGINNING: <u>181589</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8752.0</u> WH TOT	ENDING: <u>181602</u> CU FT
BLOWDOWN: <u>47</u> KLB	BLOWDOWN: <u>30</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>13</u> CU FT
BLOWDOWN: <u>3.2</u> %	BLOWDOWN: <u>2.0</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4105055</u> JEM TOT	ENDING: <u>7.7</u> FT/IN OUT
ENDING: <u>75164.3</u> HRS	ENDING: <u>74140.0</u> HRS	BEGINNING: <u>3937650</u> JEM TOT	BEGINNING: <u>7.1</u> FT/IN OUT
BEGINNING: <u>75141.3</u> HRS	BEGINNING: <u>74117.0</u> HRS	TOTAL: <u>167.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>23.0</u> HRS	TOTAL: <u>23.0</u> HRS	UTILITY IN:	EOM OUT: <u>7.58</u>
BOILER RUN TIME: <u>23.4</u> HRS	BOILER RUN TIME: <u>23.3</u> HRS	ENDING: <u>2731560</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>61.0</u> KLB/HR	AVG. STEAM FLOW: <u>82.7</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>204.0</u> TONS	APPROX REF PROC: <u>213.0</u> TONS	TOTAL: <u>3.8</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>237.4</u> TONS	REFUSE PROCESSED: <u>244.1</u> TONS	GENERATOR RUN TIME: <u>21.5</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>95.6</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2888.4</u> KLB	GROSS REFUSE REC: <u>213.00</u> TONS	KWH/TON: <u>221.2</u>	ENDING: <u>26</u> FT. OUT <u>66</u> IN OUT
TOTAL REFUSE PR. <u>431.9</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>13</u> FT. OUT <u>43</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>213.00</u> TONS		EOM OUT: <u>31.50</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,392.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>427158000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>14.89</u> TONS	
BEGINNING: <u>426857000</u> GAL		% OF REFUSE PROC: <u>3.45</u> %	
TOTAL USED: <u>301000</u> GAL			
UNIT 1 AVAILABILITY: <u>97.3</u> %	UNIT 2 AVAILABILITY: <u>97.3</u> %	TG AVAILABILITY: <u>89.6</u> %	
UNIT 1 % MCR: <u>92.1</u> %	UNIT 2 % MCR: <u>94.7</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>11.1</u>	GROSS KW/TON PR. <u>600.2</u>	
NET KWH/TON PR. <u>387.6</u>	LB LIME/TON PR.: <u>4.4</u>	TOT STM TO T/G: <u>2,835.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

unit #1 down 25 mins unit #2 down 26 mins T/G down 2hrs 23 min electric

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 29 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1501.9</u> KLB	STEAM PRODUCED: <u>1463.1</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1528.3</u> KLB	FEEDWATER USED: <u>1548.6</u> KLB	ENDING: <u>8771.0</u> WH TOT	BEGINNING: <u>181602</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8761.0</u> WH TOT	ENDING: <u>181608</u> CU FT
BLOWDOWN: <u>26</u> KLB	BLOWDOWN: <u>86</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>6</u> CU FT
BLOWDOWN: <u>1.7</u> %	BLOWDOWN: <u>5.5</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4395090</u> JEM TOT	ENDING: <u>8.2</u> FT/IN OUT
ENDING: <u>75188.3</u> HRS	ENDING: <u>74164.0</u> HRS	BEGINNING: <u>4159290</u> JEM TOT	BEGINNING: <u>7.7</u> FT/IN OUT
BEGINNING: <u>75164.3</u> HRS	BEGINNING: <u>74140.0</u> HRS	TOTAL: <u>235.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>8.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2731560</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>62.6</u> KLB/HR	AVG. STEAM FLOW: <u>61.0</u> KLB/HR	BEGINNING: <u>2731560</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>190.3</u> TONS	APPROX REF PROC: <u>212.7</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>250.3</u> TONS	REFUSE PROCESSED: <u>243.9</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>52.2</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2965.0</u> KLB	GROSS REFUSE REC: <u>224.20</u> TONS	KWH/TON: <u>126.0</u>	ENDING: <u>26</u> FT. OUT <u>8</u> IN OUT
TOTAL REFUSE PR. <u>414.2</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>26</u> FT. OUT <u>66</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
ENDING: <u>427461000</u> GAL	TOTAL REFUSE REC: <u>224.20</u> TONS	MEDICAL WASTE :	EOM OUT: <u>28.67</u>
BEGINNING: <u>427158000</u> GAL	EST PIT INVENTORY: <u>2,217.0</u> TONS	PROCESSED: <u>11.18</u> TONS	
TOTAL USED: <u>303000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.70</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>97.2</u> %	UNIT 2 % MCR: <u>94.7</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.3</u>	GROSS KW/TON PR. <u>695.3</u>	
NET KWH/TON PR. <u>569.3</u>	LB LIME/TON PR.: <u>3.8</u>	TOT STM TO T/G: <u>2,994.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 30 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1473.0</u> KLB	STEAM PRODUCED: <u>1450.7</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1510.6</u> KLB	FEEDWATER USED: <u>1524.9</u> KLB	ENDING: <u>8781.0</u> WH TOT	BEGINNING: <u>181608</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8771.0</u> WH TOT	ENDING: <u>181613</u> CU FT
BLOWDOWN: <u>38</u> KLB	BLOWDOWN: <u>74</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>5</u> CU FT
BLOWDOWN: <u>2.5</u> %	BLOWDOWN: <u>4.9</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4633360</u> JEM TOT	ENDING: <u>8.9</u> FT/IN OUT
ENDING: <u>75212.3</u> HRS	ENDING: <u>74188.0</u> HRS	BEGINNING: <u>4395090</u> JEM TOT	BEGINNING: <u>8.2</u> FT/IN OUT
BEGINNING: <u>75188.3</u> HRS	BEGINNING: <u>74164.0</u> HRS	TOTAL: <u>238.3</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>8.75</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2731560</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>61.4</u> KLB/HR	AVG. STEAM FLOW: <u>60.4</u> KLB/HR	BEGINNING: <u>2731560</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>275.1</u> TONS	APPROX REF PROC: <u>248.4</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>245.5</u> TONS	REFUSE PROCESSED: <u>241.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>49.7</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2923.7</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS	KWH/TON: <u>102.1</u>	ENDING: <u>25</u> FT. OUT <u>59</u> IN OUT
TOTAL REFUSE PR. <u>487.3</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>26</u> FT. OUT <u>8</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
ENDING: <u>427752000</u> GAL	TOTAL REFUSE REC: <u>0.00</u> TONS	MEDICAL WASTE:	EOM OUT: <u>29.92</u>
BEGINNING: <u>427461000</u> GAL	EST PIT INVENTORY: <u>1,493.0</u> TONS	PROCESSED: <u>0.00</u> TONS	
TOTAL USED: <u>291000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>95.3</u> %	UNIT 2 % MCR: <u>93.9</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>591.0</u>	
NET KWH/TON PR. <u>489.0</u>	LB LIME/TON PR.: <u>4.5</u>	TOT STM TO T/G: <u>2,924.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 31 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1430.3</u> KLB	STEAM PRODUCED: <u>1447.1</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1456.5</u> KLB	FEEDWATER USED: <u>1525.9</u> KLB	ENDING: <u>8791.0</u> WH TOT	BEGINNING: <u>181613</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8781.0</u> WH TOT	ENDING: <u>181619</u> CU FT
BLOWDOWN: <u>26</u> KLB	BLOWDOWN: <u>79</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>6</u> CU FT
BLOWDOWN: <u>1.8</u> %	BLOWDOWN: <u>5.2</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4889600</u> JEM TOT	ENDING: <u>9.8</u> FT/IN OUT
ENDING: <u>75236.3</u> HRS	ENDING: <u>74212.0</u> HRS	BEGINNING: <u>4633360</u> JEM TOT	BEGINNING: <u>8.9</u> FT/IN OUT
BEGINNING: <u>75212.3</u> HRS	BEGINNING: <u>74188.0</u> HRS	TOTAL: <u>236.2</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.67</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2731560</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.6</u> KLB/HR	AVG. STEAM FLOW: <u>60.3</u> KLB/HR	BEGINNING: <u>2731560</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>229.9</u> TONS	APPROX REF PROC: <u>216.2</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>238.4</u> TONS	REFUSE PROCESSED: <u>241.2</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>51.8</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2877.4</u> KLB	GROSS REFUSE REC: <u>315.96</u> TONS	KWH/TON: <u>116.0</u>	ENDING: <u>25</u> FT. OUT <u>39</u> IN OUT
TOTAL REFUSE PR. <u>446.1</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>25</u> FT. OUT <u>59</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
ENDING: <u>428026000</u> GAL	TOTAL REFUSE REC: <u>315.96</u> TONS	MEDICAL WASTE :	EOM OUT: <u>28.25</u>
BEGINNING: <u>427752000</u> GAL	EST PIT INVENTORY: <u>1,283.0</u> TONS	PROCESSED: <u>0.00</u> TONS	
TOTAL USED: <u>274000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>92.5</u> %	UNIT 2 % MCR: <u>93.6</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.0</u>	GROSS KW/TON PR. <u>645.7</u>	
NET KWH/TON PR. <u>529.6</u>	LB LIME/TON PR.: <u>6.3</u>	TOT STM TO T/G: <u>2,883.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JUNE 1 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1444.0</u> KLB	STEAM PRODUCED: <u>1437.8</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1479.3</u> KLB	FEEDWATER USED: <u>1515.7</u> KLB	ENDING: <u>8801.0</u> WH TOT	BEGINNING: <u>181619</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8791.0</u> WH TOT	ENDING: <u>181624</u> CU FT
BLOWDOWN: <u>35</u> KLB	BLOWDOWN: <u>78</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>5</u> CU FT
BLOWDOWN: <u>2.4</u> %	BLOWDOWN: <u>5.1</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>5107600</u> JEM TOT	ENDING: <u>10.8</u> FT/IN OUT
ENDING: <u>75260.3</u> HRS	ENDING: <u>74236.0</u> HRS	BEGINNING: <u>4869600</u> JEM TOT	BEGINNING: <u>9.8</u> FT/IN OUT
BEGINNING: <u>75236.3</u> HRS	BEGINNING: <u>74212.0</u> HRS	TOTAL: <u>238.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>10.67</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2731560</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>60.2</u> KLB/HR	AVG. STEAM FLOW: <u>59.9</u> KLB/HR	BEGINNING: <u>2731560</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>223.8</u> TONS	APPROX REF PROC: <u>210.4</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>240.7</u> TONS	REFUSE PROCESSED: <u>239.6</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>50.0</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2881.8</u> KLB	GROSS REFUSE REC: <u>767.04</u> TONS	KWH/TON: <u>112.7</u>	ENDING: <u>25</u> FT. OUT <u>6</u> IN OUT
TOTAL REFUSE PR. <u>443.6</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>25</u> FT. OUT <u>39</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>767.04</u> TONS		EOM OUT: <u>25.50</u>
WELL WATER USE:	EST PIT INVENTORY: <u>1,789.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>428333000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>9.38</u> TONS	
BEGINNING: <u>428026000</u> GAL		% OF REFUSE PROC: <u>2.11</u> %	
TOTAL USED: <u>307000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>93.4</u> %	UNIT 2 % MCR: <u>93.0</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS LB KW <u>10.0</u>	GROSS KW/TON PR. <u>649.2</u>	
NET KWH/TON PR. <u>536.5</u>	LB LIME/TON PR.: <u>7.1</u>	TOT STM TO T/G: <u>2,891.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JUNE 2, 1988

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1481.0</u> KLB	STEAM PRODUCED: <u>1467.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1515.0</u> KLB	FEEDWATER USED: <u>1548.0</u> KLB	ENDING: <u>8811.0</u> W/H TOT	BEGINNING: <u>181624</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8801.0</u> W/H TOT	ENDING: <u>181642</u> CU FT
BLOWDOWN: <u>54</u> KLB	BLOWDOWN: <u>79</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>18</u> CU FT
BLOWDOWN %: <u>3.6</u> %	BLOWDOWN %: <u>5.1</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>5347410</u> JEM TOT	ENDING: <u>12.8</u> FT/IN OUT
ENDING: <u>75284.3</u> HRS	ENDING: <u>74280.0</u> HRS	BEGINNING: <u>5107600</u> JEM TOT	BEGINNING: <u>10.8</u> FT/IN OUT
BEGINNING: <u>75280.3</u> HRS	BEGINNING: <u>74238.0</u> HRS	TOTAL: <u>239.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>12.67</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2731580</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>60.9</u> KLB/HR	AVG. STEAM FLOW: <u>61.1</u> KLB/HR	BEGINNING: <u>2731580</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>193.7</u> TONS	APPROX REF PROC: <u>208.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>652</u> LBS
REFUSE PROCESSED: <u>243.5</u> TONS	REFUSE PROCESSED: <u>244.5</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>48.2</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>118.9</u>	ENDING: <u>24</u> FT. OUT <u>88</u> IN OUT
TOTAL STEAM FLOW: <u>2928.0</u> KLB	GROSS REFUSE REC: <u>705.24</u> TONS		BEGINNING: <u>25</u> FT. OUT <u>6</u> IN OUT
TOTAL REFUSE PR: <u>402.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>18.98</u> TONS		EOM OUT: <u>29.50</u>
	TOTAL REFUSE REC: <u>686.28</u> TONS		
WELL WATER USE:	EST PIT INVENTORY: <u>1,945.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>428646000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>428330000</u> GAL		% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>313000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>94.5</u> %	UNIT 2 % MCR: <u>94.8</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR: <u>3.0</u>	LB STEAM/GROSS KW: <u>10.2</u>	GROSS KW/TON PR: <u>718.4</u>	
NET KWH/TON PR: <u>596.5</u>	LB LIME/TON PR: <u>15.6</u>	TOT STM TO T/G: <u>2,942.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JUNE 3, 1999

BOILER NO. 1 STEAM PRODUCED: <u>1549.0</u> KLB FEEDWATER USED: <u>1563.0</u> KLB BOILER BLOWDOWN: BLOWDOWN: <u>4</u> KLB BLOWDOWN: <u>0.3</u> % GRATE RUN TIME: ENDING: <u>75308.3</u> HRS BEGINNING: <u>75284.3</u> HRS TOTAL: <u>24.0</u> HRS BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>64.5</u> KLB/HR APPROX REF PROC: <u>220.0</u> TONS REFUSE PROCESSED: <u>259.2</u> TONS NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB TOTAL STEAM FLOW: <u>3088.0</u> KLB TOTAL REFUSE PR: <u>434.0</u> TONS WELL WATER USE: ENDING: <u>428953000</u> GAL BEGINNING: <u>428848000</u> GAL TOTAL USED: <u>307000</u> GAL UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>100.2</u> % LB STEAM/LB PR: <u>3.0</u> NET KW/TON PR: <u>580.7</u>	BOILER NO. 2 STEAM PRODUCED: <u>1537.0</u> KLB FEEDWATER USED: <u>1614.0</u> KLB BOILER BLOWDOWN: BLOWDOWN: <u>77</u> KLB BLOWDOWN: <u>4.8</u> % GRATE RUN TIME: ENDING: <u>74284.0</u> HRS BEGINNING: <u>74260.0</u> HRS TOTAL: <u>24.0</u> HRS BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>64.0</u> KLB/HR APPROX REF PROC: <u>197.0</u> TONS REFUSE PROCESSED: <u>258.2</u> TONS GROSS REFUSE REC: <u>717.88</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>19.27</u> TONS TOTAL REFUSE REC: <u>698.58</u> TONS EST PIT INVENTORY: <u>2,276.0</u> TONS ASH HAULED: <u>0.00</u> TONS UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>99.4</u> % LB STEAM/GROSS KW: <u>9.7</u> LB LIME/TON PR.: <u>75.8</u>	ELECTRICITY GENERATOR OUT: ENDING: <u>8822.0</u> WH TOT BEGINNING: <u>8811.0</u> WH TOT TOTAL: <u>316.8</u> MWH UTILITY OUT: ENDING: <u>5580410</u> JEM TOT BEGINNING: <u>5347410</u> JEM TOT TOTAL: <u>252.0</u> MWH UTILITY IN: ENDING: <u>2731560</u> JEM TOT BEGINNING: <u>2731560</u> JEM TOT TOTAL: <u>0.0</u> MWH GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>64.8</u> MWH KW/TON: <u>149.3</u> MEDICAL WASTE: PROCESSED: <u>19.98</u> TONS % OF REFUSE PROC: <u>3.91</u> % TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>84.1</u> % GROSS KW/TON PR: <u>730.0</u> TOT STM TO T/G: <u>3,078.0</u>	INVENTORY NATURAL GAS USAGE: BEGINNING: <u>181642</u> CU FT ENDING: <u>181642</u> CU FT TOTAL USED: <u>0</u> CU FT PEBBLE LIME: ENDING: <u>7.3</u> FT/IN OUT BEGINNING: <u>12.8</u> FT/IN OUT RECEIVED: <u>25.09</u> TONS EOM OUT: <u>7.25</u> CARBON USAGE: USAGE UNIT #1: <u>552</u> LBS USAGE UNIT #2: <u>552</u> LBS DAILY TOTAL: <u>1104</u> LBS CARBON INVENTORY: ENDING: <u>24</u> FT. OUT <u>17</u> IN OUT BEGINNING: <u>24</u> FT. OUT <u>65</u> IN OUT RECEIVED: <u>0.00</u> TONS EOM OUT: <u>25.42</u>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE January 01 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1351.5</u> KLB	STEAM PRODUCED: <u>1549.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1587.0</u> KLB	FEEDWATER USED: <u>1618.0</u> KLB	ENDING: <u>7427.0</u> WH TOT	BEGINNING: <u>173065</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7417.0</u> WH TOT	ENDING: <u>173073</u> CU FT
BLOWDOWN: <u>236</u> KLB	BLOWDOWN: <u>70</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>8</u> CU FT
BLOWDOWN: <u>14.8</u> %	BLOWDOWN: <u>4.3</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2201560</u> JEM TOT	ENDING: <u>1.1</u> FT/IN OUT
ENDING: <u>71680.7</u> HRS	ENDING: <u>70642.5</u> HRS	BEGINNING: <u>1953130</u> JEM TOT	BEGINNING: <u>1.8</u> FT/IN OUT
BEGINNING: <u>71656.7</u> HRS	BEGINNING: <u>70618.5</u> HRS	TOTAL: <u>248.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>1.08</u>
AVG. STEAM FLOW: <u>56.3</u> KLB/HR	AVG. STEAM FLOW: <u>64.5</u> KLB/HR	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>224.4</u> TONS	APPROX REF PROC: <u>244.6</u> TONS	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>225.3</u> TONS	REFUSE PROCESSED: <u>258.2</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2900.5</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS	IN PLANT USE: <u>39.6</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>469.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>84.4</u>	ENDING: <u>17</u> FT. OUT <u>92</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>17</u> FT. OUT <u>92</u> IN OUT
ENDING: <u>385101000</u> GAL	TOTAL REFUSE REC: <u>0.00</u> TONS ✓	MEDICAL WASTE:	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>384811000</u> GAL	EST PIT INVENTORY: <u>1,858.0</u> TONS ✓	PROCESSED: <u>0.00</u> TONS	EOM OUT: <u>24.67</u>
TOTAL USED: <u>290000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>87.4</u> %	UNIT 2 % MCR: <u>100.2</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.1</u>	GROSS KW/TON PR. <u>614.1</u>	
NET KWH/TON PR. <u>529.7</u>	LB LIME/TON PR.: <u>-4.7</u>	TOT STM TO T/G: <u>2,891.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

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OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE January 02 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1306.0</u> KLB	STEAM PRODUCED: <u>1541.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1538.0</u> KLB	FEEDWATER USED: <u>1620.0</u> KLB	ENDING: <u>7437.0</u> WH TOT	BEGINNING: <u>173073</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7427.0</u> WH TOT	ENDING: <u>173073</u> CU FT
BLOWDOWN: <u>232</u> KLB	BLOWDOWN: <u>79</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN %: <u>15.1</u> %	BLOWDOWN %: <u>4.9</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2440430</u> JEM TOT	ENDING: <u>2.2</u> FT/IN OUT
ENDING: <u>71704.7</u> HRS	ENDING: <u>70668.6</u> HRS	BEGINNING: <u>2201560</u> JEM TOT	BEGINNING: <u>1.8</u> FT/IN OUT
BEGINNING: <u>71680.7</u> HRS	BEGINNING: <u>70642.5</u> HRS	TOTAL: <u>238.9</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.1</u> HRS	UTILITY IN:	EOM OUT: <u>2.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>54.4</u> KLB/HR	AVG. STEAM FLOW: <u>64.2</u> KLB/HR	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>230.0</u> TONS	APPROX REF PROC: <u>248.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>217.7</u> TONS	REFUSE PROCESSED: <u>258.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>49.1</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>102.0</u>	ENDING: <u>17</u> FT. OUT <u>53</u> IN OUT
TOTAL STEAM FLOW: <u>2847.0</u> KLB	GROSS REFUSE REC: <u>378.72</u> TONS		BEGINNING: <u>17</u> FT. OUT <u>92</u> IN OUT
TOTAL REFUSE PR. <u>481.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓	MEDICAL WASTE:	EOM OUT: <u>21.42</u>
ENDING: <u>385400000</u> GAL	TOTAL REFUSE REC: <u>378.72</u> TONS ✓	PROCESSED: <u>7.15</u> TONS	
BEGINNING: <u>385101000</u> GAL	EST PIT INVENTORY: <u>1,867.0</u> TONS	% OF REFUSE PROC: <u>1.48</u> %	
TOTAL USED: <u>299000</u> GAL	ASH HAULED: <u>0.00</u> TONS		
	<u>202.01</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>84.5</u> %	UNIT 2 % MCR: <u>99.7</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.9</u>	GROSS KW/TON PR. <u>597.9</u>	
NET KWH/TON PR. <u>495.9</u>	LB LIME/TON PR.: <u>2.6</u>	TOT STM TO T/G: <u>2,849.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE January 03 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1248.9</u> KLB FEEDWATER USED: <u>1476.8</u> KLB	STEAM PRODUCED: <u>1335.9</u> KLB FEEDWATER USED: <u>1407.8</u> KLB	GENERATOR OUT: ENDING: <u>7446.0</u> WH TOT BEGINNING: <u>7437.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173073</u> CU FT ENDING: <u>173085</u> CU FT TOTAL USED: <u>12</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>228</u> KLB BLOWDOWN: <u>15.4</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>72</u> KLB BLOWDOWN: <u>5.1</u> %	UTILITY OUT: ENDING: <u>2652270</u> JEM TOT BEGINNING: <u>2440430</u> JEM TOT TOTAL: <u>211.8</u> MWH	PEBBLE LIME : ENDING: <u>2.6</u> FT/IN OUT BEGINNING: <u>2.2</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>71728.7</u> HRS BEGINNING: <u>71704.7</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>70690.8</u> HRS BEGINNING: <u>70666.8</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2600520</u> JEM TOT BEGINNING: <u>2600520</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>2.50</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	AVG. STEAM FLOW: <u>52.0</u> KLB/HR	AVG. STEAM FLOW: <u>55.7</u> KLB/HR
APPROX REF PROC: <u>219.8</u> TONS	APPROX REF PROC: <u>233.5</u> TONS	REFUSE PROCESSED: <u>208.2</u> TONS	REFUSE PROCESSED: <u>222.7</u> TONS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2584.8</u> KLB TOTAL REFUSE PR. <u>440.7</u> TONS	GROSS REFUSE REC: <u>0.00</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS TOTAL REFUSE REC: <u>0.00</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>47.4</u> MWH KWH/TON: <u>107.5</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
WELL WATER USE: ENDING: <u>385668000</u> GAL BEGINNING: <u>385400000</u> GAL TOTAL USED: <u>266000</u> GAL	EST PIT INVENTORY: <u>1,214.0</u> TONS ASH HAULED: <u>0.00</u> TONS	MEDICAL WASTE : PROCESSED: <u>9.89</u> TONS % OF REFUSE PROC: <u>2.24</u> %	CARBON INVENTORY: ENDING: <u>17</u> FT. OUT <u>46</u> IN OUT BEGINNING: <u>17</u> FT. OUT <u>53</u> IN OUT RECEIVED: <u>0.00</u> TONS EOM OUT: <u>20.83</u>
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>80.8</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>480.7</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>88.4</u> % LB STEAM/GROSS KW <u>10.0</u> LB LIME/TON PR.: <u>2.9</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>588.2</u> TOT STM TO T/G: <u>2,577.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE January 04 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>624.5</u> KLB FEEDWATER USED: <u>877.5</u> KLB	STEAM PRODUCED: <u>1347.5</u> KLB FEEDWATER USED: <u>1405.9</u> KLB	GENERATOR OUT: ENDING: <u>7451.0</u> WH TOT BEGINNING: <u>7446.0</u> WH TOT TOTAL: <u>144.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173085</u> CU FT ENDING: <u>173452</u> CU FT TOTAL USED: <u>367</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>53</u> KLB BLOWDOWN : <u>7.8</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>58</u> KLB BLOWDOWN : <u>4.2</u> %	UTILITY OUT: ENDING: <u>2776980</u> JEM TOT BEGINNING: <u>2652270</u> JEM TOT TOTAL: <u>124.7</u> MWH	PEBBLE LIME : ENDING: <u>2.2</u> FT/IN OUT BEGINNING: <u>2.6</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>71745.7</u> HRS BEGINNING: <u>71728.7</u> HRS TOTAL: <u>17.0</u> HRS	GRATE RUN TIME: ENDING: <u>70714.6</u> HRS BEGINNING: <u>70690.6</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2600520</u> JEM TOT BEGINNING: <u>2600520</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>2.17</u>
BOILER RUN TIME: <u>9.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>19.3</u> MWH KWH/TON: <u>88.4</u>	CARBON USAGE: USAGE UNIT #1: <u>101</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>370</u> LBS
AVG. STEAM FLOW: <u>69.4</u> KLB/HR	AVG. STEAM FLOW: <u>56.1</u> KLB/HR		CARBON INVENTORY: ENDING: <u>17</u> FT. OUT <u>35</u> IN OUT BEGINNING: <u>17</u> FT. OUT <u>46</u> IN OUT RECEIVED: <u>0.00</u> TONS
APPROX REF PROC: <u>68.7</u> TONS	APPROX REF PROC: <u>213.5</u> TONS		EOM OUT: <u>19.92</u>
REFUSE PROCESSED: <u>104.1</u> TONS	REFUSE PROCESSED: <u>224.6</u> TONS		
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>1972.0</u> KLB TOTAL REFUSE PR. <u>282.2</u> TONS	GROSS REFUSE REC: <u>734.74</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>15.55</u> TONS TOTAL REFUSE REC: <u>719.19</u> TONS <i>713.42</i>	MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	
WELL WATER USE: ENDING: <u>385889000</u> GAL BEGINNING: <u>385666000</u> GAL TOTAL USED: <u>223000</u> GAL	EST PIT INVENTORY: <u>1,692.0</u> TONS ASH HAULED: <u>0.00</u> TONS <i>148.95</i>		
UNIT 1 AVAILABILITY: <u>37.5</u> % UNIT 1 % MCR: <u>40.4</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>441.9</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>87.2</u> % LB STEAM/GROSS KW <u>13.7</u> LB LIME/TON PR.: <u>-4.5</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>38.2</u> % GROSS KW/TON PR. <u>510.3</u> TOT STM TO T/G: <u>1,683.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1blr. down econo. drain line repair

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE January 05 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1328.5</u> KLB	STEAM PRODUCED: <u>1319.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1545.5</u> KLB	FEEDWATER USED: <u>1564.0</u> KLB	ENDING: <u>7461.0</u> WH TOT	BEGINNING: <u>173452</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7451.0</u> WH TOT	ENDING: <u>173453</u> CU FT
BLOWDOWN: <u>217</u> KLB	BLOWDOWN: <u>245</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>14.0</u> %	BLOWDOWN: <u>15.7</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3014000</u> JEM TOT	ENDING: <u>2.9</u> FT/IN OUT
ENDING: <u>71769.7</u> HRS	ENDING: <u>70738.6</u> HRS	BEGINNING: <u>2776980</u> JEM TOT	BEGINNING: <u>2.6</u> FT/IN OUT
BEGINNING: <u>71745.7</u> HRS	BEGINNING: <u>70714.6</u> HRS	TOTAL: <u>237.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>2.75</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2800520</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.4</u> KLB/HR	AVG. STEAM FLOW: <u>55.0</u> KLB/HR	BEGINNING: <u>2800520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>213.7</u> TONS	APPROX REF PROC: <u>223.9</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>221.4</u> TONS	REFUSE PROCESSED: <u>219.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>51.0</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2647.5</u> KLB	GROSS REFUSE REC: <u>758.52</u> TONS	KWH/TON: <u>115.6</u>	ENDING: <u>17</u> FT. OUT <u>29</u> IN OUT
TOTAL REFUSE PR. <u>440.8</u> TONS	NON PROCESSED: <u>0.00</u> TONS	MEDICAL WASTE :	BEGINNING: <u>17</u> FT. OUT <u>35</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>17.87</u> TONS ✓	PROCESSED: <u>3.16</u> TONS	RECEIVED: <u>0.00</u> TONS
ENDING: <u>386168000</u> GAL	TOTAL REFUSE REC: <u>740.65</u> TONS ✓	% OF REFUSE PROC: <u>0.72</u> %	EOM OUT: <u>19.42</u>
BEGINNING: <u>385889000</u> GAL	EST PIT INVENTORY: <u>1,990.0</u> TONS	UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %
TOTAL USED: <u>279000</u> GAL	ASH HAULED: <u>0.00</u> TONS	UNIT 1 % MCR: <u>86.0</u> %	UNIT 2 % MCR: <u>85.3</u> %
	<u>153.73</u>	LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.2</u>
		NET KWH/TON PR. <u>537.7</u>	LB LIME/TON PR.: <u>2.1</u>
		TG AVAILABILITY: <u>100.0</u> %	TG % MCR: <u>76.4</u> %
		GROSS KW/TON PR. <u>653.3</u>	TOT STM TO T/G: <u>2,850.0</u>

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE January 08 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1164.0</u> KLB	STEAM PRODUCED: <u>1547.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1356.0</u> KLB	FEEDWATER USED: <u>1569.0</u> KLB	ENDING: <u>7470.0</u> WH TOT	BEGINNING: <u>173453</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7481.0</u> WH TOT	ENDING: <u>173453</u> CU FT
BLOWDOWN: <u>192</u> KLB	BLOWDOWN: <u>22</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN %: <u>14.2</u> %	BLOWDOWN %: <u>1.4</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3234510</u> JEM TOT	ENDING: <u>0.8</u> FT/IN OUT
ENDING: <u>71793.5</u> HRS	ENDING: <u>70762.6</u> HRS	BEGINNING: <u>3014000</u> JEM TOT	BEGINNING: <u>2.9</u> FT/IN OUT
BEGINNING: <u>71769.7</u> HRS	BEGINNING: <u>70738.8</u> HRS	TOTAL: <u>220.5</u> MWH	RECEIVED: <u>25.57</u> TONS
TOTAL: <u>23.8</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>0.67</u>
AVG. STEAM FLOW: <u>48.5</u> KLB/HR	AVG. STEAM FLOW: <u>64.5</u> KLB/HR	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>189.9</u> TONS	APPROX REF PROC: <u>234.1</u> TONS	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>194.0</u> TONS	REFUSE PROCESSED: <u>257.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2711.0</u> KLB	GROSS REFUSE REC: <u>584.49</u> TONS	IN PLANT USE: <u>38.7</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>424.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>91.2</u>	ENDING: <u>17</u> FT. OUT <u>29</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>17</u> FT. OUT <u>29</u> IN OUT
ENDING: <u>386436000</u> GAL	TOTAL REFUSE REC: <u>584.49</u> TONS ✓	MEDICAL WASTE:	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>386188000</u> GAL	EST PIT INVENTORY: <u>2,139.0</u> TONS	PROCESSED: <u>0.00</u> TONS	EOM OUT: <u>19.42</u>
TOTAL USED: <u>268000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.00</u> %	
	<u>150.72</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>75.3</u> %	UNIT 2 % MCR: <u>100.1</u> %	TG % MCR: <u>88.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.5</u>	GROSS KW/TON PR. <u>611.3</u>	
NET KWH/TON PR. <u>520.1</u>	LB LIME/TON PR.: <u>105.1</u>	TOT STM TO T/G: <u>2,685.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE January 07, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1077.0</u> KLB	STEAM PRODUCED: <u>1568.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1257.0</u> KLB	FEEDWATER USED: <u>1592.0</u> KLB	ENDING: <u>7479.0</u> WH TOT	BEGINNING: <u>173453</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7470.0</u> WH TOT	ENDING: <u>173454</u> CU FT
BLOWDOWN: <u>180</u> KLB	BLOWDOWN: <u>24</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>14.3</u> %	BLOWDOWN: <u>1.5</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3447350</u> JEM TOT	ENDING: <u>0.8</u> FT/IN OUT
ENDING: <u>71817.2</u> HRS	ENDING: <u>70786.5</u> HRS	BEGINNING: <u>3234510</u> JEM TOT	BEGINNING: <u>0.8</u> FT/IN OUT
BEGINNING: <u>71793.5</u> HRS	BEGINNING: <u>70762.6</u> HRS	TOTAL: <u>212.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>23.7</u> HRS	TOTAL: <u>23.9</u> HRS	UTILITY IN:	EOM OUT: <u>0.67</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>44.9</u> KLB/HR	AVG. STEAM FLOW: <u>65.3</u> KLB/HR	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>175.0</u> TONS	APPROX REF PROC: <u>230.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>179.5</u> TONS	REFUSE PROCESSED: <u>261.3</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>48.4</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>114.5</u>	ENDING: <u>17</u> FT. OUT <u>20</u> IN OUT
TOTAL STEAM FLOW: <u>2645.0</u> KLB	GROSS REFUSE REC: <u>551.76</u> TONS		BEGINNING: <u>17</u> FT. OUT <u>29</u> IN OUT
TOTAL REFUSE PR. <u>405.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>18.67</u>
	TOTAL REFUSE REC: <u>551.76</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>2,392.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>386709000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>386436000</u> GAL	<u>156.29</u>	% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>273000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>69.7</u> %	UNIT 2 % MCR: <u>101.4</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>640.0</u>	
NET KWH/TON PR. <u>525.5</u>	LB LIME/TON PR.: <u>0.0</u>	TOT STM TO T/G: <u>2,600.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE January 08, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1064.0</u> KLB	STEAM PRODUCED: <u>1560.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1238.0</u> KLB	FEEDWATER USED: <u>1584.0</u> KLB	ENDING: <u>7488.0</u> WH TOT	BEGINNING: <u>173454</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7479.0</u> WH TOT	ENDING: <u>173454</u> CU FT
BLOWDOWN: <u>174</u> KLB	BLOWDOWN: <u>24</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>14.1</u> %	BLOWDOWN: <u>1.5</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3660200</u> JEM TOT	ENDING: <u>1.0</u> FT/IN OUT
ENDING: <u>71841.2</u> HRS	ENDING: <u>70810.5</u> HRS	BEGINNING: <u>3447350</u> JEM TOT	BEGINNING: <u>0.8</u> FT/IN OUT
BEGINNING: <u>71817.2</u> HRS	BEGINNING: <u>70786.5</u> HRS	TOTAL: <u>212.9</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>1.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>44.3</u> KLB/HR	AVG. STEAM FLOW: <u>65.0</u> KLB/HR	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>175.0</u> TONS	APPROX REF PROC: <u>230.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>177.3</u> TONS	REFUSE PROCESSED: <u>260.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>46.3</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2624.0</u> KLB	GROSS REFUSE REC: <u>558.17</u> TONS	KWH/TON: <u>114.4</u>	ENDING: <u>16</u> FT. OUT <u>90</u> IN OUT
TOTAL REFUSE PR. <u>405.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>17</u> FT. OUT <u>20</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>558.17</u> TONS ✓		EOM OUT: <u>23.50</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,451.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>386983000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>386709000</u> GAL	<u>72.76</u>	% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>274000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>68.8</u> %	UNIT 2 % MCR: <u>100.9</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.1</u>	GROSS KW/TON PR. <u>640.0</u>	
NET KWH/TON PR. <u>525.6</u>	LB LIME/TON PR.: <u>1.6</u>	TOT STM TO T/G: <u>2,584.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE January 09, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1123.0</u> KLB	STEAM PRODUCED: <u>1512.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1265.0</u> KLB	FEEDWATER USED: <u>1536.0</u> KLB	ENDING: <u>7497.0</u> WH TOT	BEGINNING: <u>173454</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7488.0</u> WH TOT	ENDING: <u>173455</u> CU FT
BLOWDOWN: <u>142</u> KLB	BLOWDOWN: <u>24</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>11.2</u> %	BLOWDOWN: <u>1.6</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3876650</u> JEM TOT	ENDING: <u>1.5</u> FT/IN OUT
ENDING: <u>71865.2</u> HRS	ENDING: <u>70834.4</u> HRS	BEGINNING: <u>3660200</u> JEM TOT	BEGINNING: <u>1.0</u> FT/IN OUT
BEGINNING: <u>71841.2</u> HRS	BEGINNING: <u>70810.5</u> HRS	TOTAL: <u>216.5</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.9</u> HRS	UTILITY IN:	EOM OUT: <u>1.42</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>46.8</u> KLB/HR	AVG. STEAM FLOW: <u>63.0</u> KLB/HR	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>177.0</u> TONS	APPROX REF PROC: <u>242.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>187.2</u> TONS	REFUSE PROCESSED: <u>252.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>42.7</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>100.4</u>	ENDING: <u>18</u> FT. OUT <u>80</u> IN OUT
TOTAL STEAM FLOW: <u>2835.0</u> KLB	GROSS REFUSE REC: <u>285.69</u> TONS		BEGINNING: <u>18</u> FT. OUT <u>90</u> IN OUT
TOTAL REFUSE PR. <u>425.8</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>19.20</u> TONS ✓		EOM OUT: <u>22.67</u>
	TOTAL REFUSE REC: <u>266.49</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>2,217.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>387255000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>6.78</u> TONS	
BEGINNING: <u>386983000</u> GAL		% OF REFUSE PROC: <u>1.59</u> %	
TOTAL USED: <u>272000</u> GAL	<u>27.06</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>72.7</u> %	UNIT 2 % MCR: <u>97.8</u> %	TG % MCR: <u>88.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>608.8</u>	
NET KWH/TON PR. <u>508.4</u>	LB LIME/TON PR.: <u>3.7</u>	TOT STM TO T/G: <u>2,620.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE January 10, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1325.0</u> KLB	STEAM PRODUCED: <u>1446.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1540.0</u> KLB	FEEDWATER USED: <u>1470.0</u> KLB	ENDING: <u>7507.0</u> WH TOT	BEGINNING: <u>173455</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7497.0</u> WH TOT	ENDING: <u>173455</u> CU FT
BLOWDOWN: <u>215</u> KLB	BLOWDOWN: <u>24</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>14.0</u> %	BLOWDOWN: <u>1.6</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4108680</u> JEM TOT	ENDING: <u>1.7</u> FT/IN OUT
ENDING: <u>71889.2</u> HRS	ENDING: <u>70858.4</u> HRS	BEGINNING: <u>3876650</u> JEM TOT	BEGINNING: <u>1.5</u> FT/IN OUT
BEGINNING: <u>71865.2</u> HRS	BEGINNING: <u>70834.4</u> HRS	TOTAL: <u>232.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>1.58</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.2</u> KLB/HR	AVG. STEAM FLOW: <u>60.3</u> KLB/HR	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>241.0</u> TONS	APPROX REF PROC: <u>232.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>220.8</u> TONS	REFUSE PROCESSED: <u>241.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>56.0</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>121.2</u>	ENDING: <u>16</u> FT. OUT <u>80</u> IN OUT
TOTAL STEAM FLOW: <u>2771.0</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS		BEGINNING: <u>16</u> FT. OUT <u>80</u> IN OUT
TOTAL REFUSE PR. <u>461.8</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>22.67</u>
	TOTAL REFUSE REC: <u>0.00</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>1,834.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>387541000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>387255000</u> GAL		% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>286000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.7</u> %	UNIT 2 % MCR: <u>93.6</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.6</u>	GROSS KW/TON PR. <u>623.6</u>	
NET KWH/TON PR. <u>502.4</u>	LB LIME/TON PR.: <u>1.4</u>	TOT STM TO T/G: <u>2,755.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 11, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1417.1</u> KLB	STEAM PRODUCED: <u>1447.8</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1644.3</u> KLB	FEEDWATER USED: <u>1472.8</u> KLB	ENDING: <u>7517.0</u> WH TOT	BEGINNING: <u>173455</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7507.0</u> WH TOT	ENDING: <u>173458</u> CU FT
BLOWDOWN: <u>227</u> KLB	BLOWDOWN: <u>25</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>13.8</u> %	BLOWDOWN: <u>1.7</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4350380</u> JEM TOT	ENDING: <u>2.8</u> FT/IN OUT
ENDING: <u>71913.2</u> HRS	ENDING: <u>70882.4</u> HRS	BEGINNING: <u>4108680</u> JEM TOT	BEGINNING: <u>1.7</u> FT/IN OUT
BEGINNING: <u>71889.2</u> HRS	BEGINNING: <u>70858.4</u> HRS	TOTAL: <u>241.7</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>2.67</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.0</u> KLB/HR	AVG. STEAM FLOW: <u>60.3</u> KLB/HR	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>250.6</u> TONS	APPROX REF PROC: <u>222.9</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>236.2</u> TONS	REFUSE PROCESSED: <u>241.3</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>46.3</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>97.8</u>	ENDING: <u>16</u> FT. OUT <u>25</u> IN OUT
TOTAL STEAM FLOW: <u>2864.9</u> KLB	GROSS REFUSE REC: <u>668.06</u> TONS		BEGINNING: <u>18</u> FT. OUT <u>80</u> IN OUT
TOTAL REFUSE PR. <u>473.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>18.08</u>
	TOTAL REFUSE REC: <u>668.06</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>1,750.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>387826000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>387541000</u> GAL		% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>285000</u> GAL	<u>127.17</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>91.7</u> %	UNIT 2 % MCR: <u>93.7</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.9</u>	GROSS KW/TON PR. <u>608.2</u>	
NET KWH/TON PR. <u>510.5</u>	LB LIME/TON PR.: <u>7.3</u>	TOT STM TO T/G: <u>2,876.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 12, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1434.1</u> KLB	STEAM PRODUCED: <u>1453.7</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1665.5</u> KLB	FEEDWATER USED: <u>1477.5</u> KLB	ENDING: <u>7527.0</u> WH TOT	BEGINNING: <u>173456</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7517.0</u> WH TOT	ENDING: <u>173456</u> CU FT
BLOWDOWN: <u>231</u> KLB	BLOWDOWN: <u>24</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>13.9</u> %	BLOWDOWN: <u>1.6</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4590110</u> JEM TOT	ENDING: <u>3.8</u> FT/IN OUT
ENDING: <u>71937.2</u> HRS	ENDING: <u>70906.4</u> HRS	BEGINNING: <u>4350380</u> JEM TOT	BEGINNING: <u>2.8</u> FT/IN OUT
BEGINNING: <u>71913.2</u> HRS	BEGINNING: <u>70882.4</u> HRS	TOTAL: <u>239.7</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>3.67</u>
AVG. STEAM FLOW: <u>59.8</u> KLB/HR	AVG. STEAM FLOW: <u>60.6</u> KLB/HR	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>235.9</u> TONS	APPROX REF PROC: <u>219.2</u> TONS	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>239.0</u> TONS	REFUSE PROCESSED: <u>242.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2887.8</u> KLB	GROSS REFUSE REC: <u>680.62</u> TONS	IN PLANT USE: <u>48.3</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>457.3</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>105.6</u>	ENDING: <u>16</u> FT. OUT <u>25</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓	MEDICAL WASTE :	BEGINNING: <u>16</u> FT. OUT <u>25</u> IN OUT
ENDING: <u>388112000</u> GAL	TOTAL REFUSE REC: <u>680.62</u> TONS ✓	PROCESSED: <u>2.14</u> TONS	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>387826000</u> GAL	EST PIT INVENTORY: <u>1,984.0</u> TONS	% OF REFUSE PROC: <u>0.47</u> %	EOM OUT: <u>18.08</u>
TOTAL USED: <u>286000</u> GAL	ASH HAULED: <u>0.00</u> TONS		
	<u>160.15</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>92.8</u> %	UNIT 2 % MCR: <u>94.1</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.0</u>	GROSS KW/TON PR. <u>629.8</u>	
NET KWH/TON PR. <u>524.2</u>	LB LIME/TON PR.: <u>6.9</u>	TOT STM TO T/G: <u>2,884.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE January 13 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1424.7</u> KLB	STEAM PRODUCED: <u>1242.6</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1654.2</u> KLB	FEEDWATER USED: <u>1269.7</u> KLB	ENDING: <u>7536.0</u> WH TOT	BEGINNING: <u>173456</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7527.0</u> WH TOT	ENDING: <u>173456</u> CU FT
BLOWDOWN: <u>230</u> KLB	BLOWDOWN: <u>27</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>13.9</u> %	BLOWDOWN: <u>2.1</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4805300</u> JEM TOT	ENDING: <u>4.2</u> FT/IN OUT
ENDING: <u>71961.2</u> HRS	ENDING: <u>70930.4</u> HRS	BEGINNING: <u>4590110</u> JEM TOT	BEGINNING: <u>3.8</u> FT/IN OUT
BEGINNING: <u>71937.2</u> HRS	BEGINNING: <u>70906.4</u> HRS	TOTAL: <u>215.2</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>4.17</u>
AVG. STEAM FLOW: <u>59.4</u> KLB/HR	AVG. STEAM FLOW: <u>51.8</u> KLB/HR	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>246.6</u> TONS	APPROX REF PROC: <u>193.3</u> TONS	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>237.4</u> TONS	REFUSE PROCESSED: <u>207.1</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2667.3</u> KLB	GROSS REFUSE REC: <u>577.10</u> TONS	IN PLANT USE: <u>44.0</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>439.9</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>100.1</u>	ENDING: <u>16</u> FT. OUT <u>4</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>16</u> FT. OUT <u>25</u> IN OUT
	TOTAL REFUSE REC: <u>577.10</u> TONS <u>577.08</u>		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	EST PIT INVENTORY: <u>2,023.0</u> TONS	MEDICAL WASTE :	EOM OUT: <u>16.33</u>
ENDING: <u>388388000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>388112000</u> GAL	<u>149.13</u>	% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>276000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>92.2</u> %	UNIT 2 % MCR: <u>80.4</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.3</u>	GROSS KW/TON PR. <u>589.3</u>	
NET KWH/TON PR. <u>489.2</u>	LB LIME/TON PR.: <u>2.9</u>	TOT STM TO T/G: <u>2,653.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 14 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1444.7</u> KLB FEEDWATER USED: <u>1677.5</u> KLB	STEAM PRODUCED: <u>1206.1</u> KLB FEEDWATER USED: <u>1231.4</u> KLB	GENERATOR OUT: ENDING: <u>7545.0</u> WH TOT BEGINNING: <u>7536.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173456</u> CU FT ENDING: <u>173456</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>233</u> KLB BLOWDOWN : <u>13.9</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>25</u> KLB BLOWDOWN : <u>2.1</u> %	UTILITY OUT: ENDING: <u>5019100</u> JEM TOT BEGINNING: <u>4805300</u> JEM TOT TOTAL: <u>213.8</u> MWH	PEBBLE LIME : ENDING: <u>4.2</u> FT/IN OUT BEGINNING: <u>4.2</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>71985.2</u> HRS BEGINNING: <u>71961.2</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>70954.4</u> HRS BEGINNING: <u>70930.4</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2600520</u> JEM TOT BEGINNING: <u>2600520</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>4.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>45.4</u> MWH KWH/TON: <u>107.3</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
AVG. STEAM FLOW: <u>60.2</u> KLB/HR	AVG. STEAM FLOW: <u>50.3</u> KLB/HR		CARBON INVENTORY: ENDING: <u>16</u> FT. OUT <u>5</u> IN OUT BEGINNING: <u>16</u> FT. OUT <u>4</u> IN OUT RECEIVED: <u>0.00</u> TONS EOM OUT: <u>16.42</u>
APPROX REF PROC: <u>245.0</u> TONS	APPROX REF PROC: <u>178.0</u> TONS		
REFUSE PROCESSED: <u>240.8</u> TONS	REFUSE PROCESSED: <u>201.0</u> TONS		
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2650.8</u> KLB TOTAL REFUSE PR. <u>423.0</u> TONS	GROSS REFUSE REC: <u>508.40</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>17.15</u> TONS ✓ TOTAL REFUSE REC: <u>491.25</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	
WELL WATER USE: ENDING: <u>388679000</u> GAL BEGINNING: <u>388388000</u> GAL TOTAL USED: <u>291000</u> GAL	EST PIT INVENTORY: <u>2,217.0</u> TONS ✓ ASH HAULED: <u>0.00</u> TONS ✓		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>93.5</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>505.4</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>78.0</u> % LB STEAM/GROSS KW <u>10.2</u> LB LIME/TON PR.: <u>0.0</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>612.8</u> TOT STM TO T/G: <u>2,628.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 15, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1449.0</u> KLB	STEAM PRODUCED: <u>1457.5</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1685.0</u> KLB	FEEDWATER USED: <u>1481.5</u> KLB	ENDING: <u>7555.0</u> WH TOT	BEGINNING: <u>173456</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7545.0</u> WH TOT	ENDING: <u>173464</u> CU FT
BLOWDOWN: <u>236</u> KLB	BLOWDOWN: <u>24</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>8</u> CU FT
BLOWDOWN: <u>14.0</u> %	BLOWDOWN: <u>1.6</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>5260700</u> JEM TOT	ENDING: <u>4.4</u> FT/IN OUT
ENDING: <u>72009.2</u> HRS	ENDING: <u>70978.4</u> HRS	BEGINNING: <u>5019100</u> JEM TOT	BEGINNING: <u>4.2</u> FT/IN OUT
BEGINNING: <u>71985.2</u> HRS	BEGINNING: <u>70954.4</u> HRS	TOTAL: <u>241.6</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>4.33</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>60.4</u> KLB/HR	AVG. STEAM FLOW: <u>60.7</u> KLB/HR	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>213.0</u> TONS	APPROX REF PROC: <u>218.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>241.5</u> TONS	REFUSE PROCESSED: <u>242.9</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>46.4</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>105.9</u>	ENDING: <u>16</u> FT. OUT <u>3</u> IN OUT
TOTAL STEAM FLOW: <u>2906.5</u> KLB	GROSS REFUSE REC: <u>557.74</u> TONS		BEGINNING: <u>16</u> FT. OUT <u>4</u> IN OUT
TOTAL REFUSE PR. <u>438.2</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>21.02</u> TONS ✓		EOM OUT: <u>16.25</u>
	TOTAL REFUSE REC: <u>536.72</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>2,276.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>388981000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>7.20</u> TONS	
BEGINNING: <u>388679000</u> GAL		% OF REFUSE PROC: <u>1.64</u> %	
TOTAL USED: <u>302000</u> GAL	<u>162.95</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>93.8</u> %	UNIT 2 % MCR: <u>94.3</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.1</u>	GROSS KW/TON PR. <u>657.2</u>	
NET KWH/TON PR. <u>551.3</u>	LB LIME/TON PR.: <u>1.4</u>	TOT STM TO T/G: <u>2,803.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 18, 1989

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1449.1</u> KLB	STEAM PRODUCED: <u>1470.5</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1688.2</u> KLB	FEEDWATER USED: <u>1495.5</u> KLB	ENDING: <u>7565.0</u> WH TOT	BEGINNING: <u>173464</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7555.0</u> WH TOT	ENDING: <u>173470</u> CU FT
BLOWDOWN: <u>239</u> KLB	BLOWDOWN: <u>25</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>6</u> CU FT
BLOWDOWN : <u>14.2</u> %	BLOWDOWN : <u>1.7</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>5503360</u> JEM TOT	ENDING: <u>5.1</u> FT/IN OUT
ENDING: <u>72033.2</u> HRS	ENDING: <u>71002.4</u> HRS	BEGINNING: <u>5260700</u> JEM TOT	BEGINNING: <u>4.4</u> FT/IN OUT
BEGINNING: <u>72009.2</u> HRS	BEGINNING: <u>70978.4</u> HRS	TOTAL: <u>242.7</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>5.08</u>
AVG. STEAM FLOW: <u>60.4</u> KLB/HR	AVG. STEAM FLOW: <u>61.3</u> KLB/HR	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>213.9</u> TONS	APPROX REF PROC: <u>192.7</u> TONS	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>241.5</u> TONS	REFUSE PROCESSED: <u>245.1</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2919.8</u> KLB	GROSS REFUSE REC: <u>201.38</u> TONS	IN PLANT USE: <u>45.3</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>406.8</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>111.5</u>	ENDING: <u>18</u> FT. OUT <u>1</u> IN OUT
<i>48681</i>	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>16</u> FT. OUT <u>3</u> IN OUT
WELL WATER USE:	TOTAL REFUSE REC: <u>201.38</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
ENDING: <u>389271000</u> GAL	EST PIT INVENTORY: <u>1,809.0</u> TONS	MEDICAL WASTE :	EOM OUT: <u>18.08</u>
BEGINNING: <u>388981000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.21</u> TONS	
TOTAL USED: <u>290000</u> GAL	<i>130.23</i>	% OF REFUSE PROC: <u>0.05</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>93.8</u> %	UNIT 2 % MCR: <u>95.1</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.1</u>	GROSS KW/TON PR. <u>707.9</u>	
NET KWH/TON PR. <u>596.5</u>	LB LIME/TON PR.: <u>5.4</u>	TOT STM TO T/G: <u>2,906.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 17, 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1401.1</u> KLB FEEDWATER USED: <u>1651.3</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>250</u> KLB BLOWDOWN : <u>15.2</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72057.2</u> HRS BEGINNING: <u>72033.2</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>58.4</u> KLB/HR APPROX REF PROC: <u>197.8</u> TONS REFUSE PROCESSED: <u>233.5</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2845.8</u> KLB TOTAL REFUSE PR. <u>387.6</u> TONS <i>474.3</i></p> <p>WELL WATER USE: ENDING: <u>389573000</u> GAL BEGINNING: <u>389271000</u> GAL TOTAL USED: <u>302000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>90.7</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>806.0</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1444.7</u> KLB FEEDWATER USED: <u>1469.5</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>25</u> KLB BLOWDOWN : <u>1.7</u> %</p> <p>GRATE RUN TIME: ENDING: <u>71026.4</u> HRS BEGINNING: <u>71002.4</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>60.2</u> KLB/HR APPROX REF PROC: <u>189.8</u> TONS REFUSE PROCESSED: <u>240.8</u> TONS</p> <p>GROSS REFUSE REC: <u>0.00</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>0.00</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>1,361.0</u> TONS ASH HAULED: <u>0.00</u> TONS ✓</p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>93.5</u> % LB STEAM/GROSS KW <u>11.0</u> LB LIME/TON PR.: <u>7.3</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>7574.0</u> WH TOT BEGINNING: <u>7565.0</u> WH TOT TOTAL: <u>259.2</u> MWH</p> <p>UTILITY OUT: ENDING: <u>5738230</u> JEM TOT BEGINNING: <u>5503360</u> JEM TOT TOTAL: <u>234.9</u> MWH</p> <p>UTILITY IN: ENDING: <u>2600520</u> JEM TOT BEGINNING: <u>2600520</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>24.3</u> MWH KWH/TON: <u>62.8</u></p> <p>MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>668.7</u> TOT STM TO T/G: <u>2,843.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173470</u> CU FT ENDING: <u>173470</u> CU FT TOTAL USED: <u>0</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>6.0</u> FT/IN OUT BEGINNING: <u>5.1</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>6.00</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>15</u> FT. OUT <u>85</u> IN OUT BEGINNING: <u>16</u> FT. OUT <u>1</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>22.08</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 18, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1294.1</u> KLB	STEAM PRODUCED: <u>1392.4</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1593.1</u> KLB	FEEDWATER USED: <u>1417.3</u> KLB	ENDING: <u>7584.0</u> WH TOT	BEGINNING: <u>173470</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7574.0</u> WH TOT	ENDING: <u>173470</u> CU FT
BLOWDOWN: <u>299</u> KLB	BLOWDOWN: <u>25</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>18.8</u> %	BLOWDOWN: <u>1.8</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>5963210</u> JEM TOT	ENDING: <u>7.2</u> FT/IN OUT
ENDING: <u>72081.2</u> HRS	ENDING: <u>71050.4</u> HRS	BEGINNING: <u>5738230</u> JEM TOT	BEGINNING: <u>6.0</u> FT/IN OUT
BEGINNING: <u>72057.2</u> HRS	BEGINNING: <u>71026.4</u> HRS	TOTAL: <u>225.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>7.17</u>
AVG. STEAM FLOW: <u>53.9</u> KLB/HR	AVG. STEAM FLOW: <u>58.0</u> KLB/HR	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>214.4</u> TONS	APPROX REF PROC: <u>199.5</u> TONS	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>215.7</u> TONS	REFUSE PROCESSED: <u>232.1</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2686.5</u> KLB	GROSS REFUSE REC: <u>594.08</u> TONS	IN PLANT USE: <u>63.0</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>413.9</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>152.3</u>	ENDING: <u>15</u> FT. OUT <u>76</u> IN OUT
<u>447.8</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>15</u> FT. OUT <u>85</u> IN OUT
WELL WATER USE:	TOTAL REFUSE REC: <u>594.08</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
ENDING: <u>389858000</u> GAL	EST PIT INVENTORY: <u>1,595.0</u> TONS	MEDICAL WASTE:	EOM OUT: <u>21.33</u>
BEGINNING: <u>389573000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.00</u> TONS	
TOTAL USED: <u>285000</u> GAL	<u>125.38</u>	% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>83.7</u> %	UNIT 2 % MCR: <u>90.1</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.3</u>	GROSS KW/TON PR. <u>695.9</u>	
NET KWH/TON PR. <u>543.8</u>	LB LIME/TON PR.: <u>9.1</u>	TOT STM TO T/G: <u>2,750.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 19, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1308.5</u> KLB FEEDWATER USED: <u>1580.6</u> KLB	STEAM PRODUCED: <u>1367.8</u> KLB FEEDWATER USED: <u>1408.2</u> KLB	GENERATOR OUT: ENDING: <u>7593.0</u> WH TOT BEGINNING: <u>7584.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173470</u> CU FT ENDING: <u>173473</u> CU FT TOTAL USED: <u>3</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>272</u> KLB BLOWDOWN: <u>17.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>38</u> KLB BLOWDOWN: <u>2.7</u> %	UTILITY OUT: ENDING: <u>6183430</u> JEM TOT BEGINNING: <u>5983210</u> JEM TOT TOTAL: <u>220.2</u> MWH	PEBBLE LIME : ENDING: <u>8.2</u> FT/IN OUT BEGINNING: <u>7.2</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>72105.2</u> HRS BEGINNING: <u>72081.2</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>71074.4</u> HRS BEGINNING: <u>71050.4</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2600520</u> JEM TOT BEGINNING: <u>2600520</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>8.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>54.5</u> KLB/HR	AVG. STEAM FLOW: <u>57.0</u> KLB/HR	IN PLANT USE: <u>39.0</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>200.6</u> TONS	APPROX REF PROC: <u>187.7</u> TONS	KWH/TON: <u>100.3</u>	CARBON INVENTORY: ENDING: <u>15</u> FT. OUT <u>61</u> IN OUT BEGINNING: <u>15</u> FT. OUT <u>76</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>218.1</u> TONS	REFUSE PROCESSED: <u>228.0</u> TONS		EOM OUT: <u>20.08</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2676.3</u> KLB TOTAL REFUSE PR. <u>388.5</u> TONS <i>444.25</i>	GROSS REFUSE REC: <u>708.95</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>19.81</u> TONS ✓ TOTAL REFUSE REC: <u>687.14</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>0.18</u> TONS % OF REFUSE PROC: <u>0.05</u> %	
WELL WATER USE: ENDING: <u>390138000</u> GAL BEGINNING: <u>389858000</u> GAL TOTAL USED: <u>280000</u> GAL	EST PIT INVENTORY: <u>1,864.0</u> TONS ASH HAULED: <u>0.00</u> TONS <i>154.35</i>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>84.7</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>566.8</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>88.5</u> % LB STEAM/GROSS KW <u>10.3</u> LB LIME/TON PR.: <u>8.1</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>667.2</u> TOT STM TO T/G: <u>2,682.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 20, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1339.2</u> KLB	STEAM PRODUCED: <u>1387.5</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1575.1</u> KLB	FEEDWATER USED: <u>1432.6</u> KLB	ENDING: <u>7602.0</u> WH TOT	BEGINNING: <u>173473</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7593.0</u> WH TOT	ENDING: <u>173487</u> CU FT
BLOWDOWN: <u>238</u> KLB	BLOWDOWN: <u>45</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>14</u> CU FT
BLOWDOWN %: <u>15.0</u> %	BLOWDOWN %: <u>3.1</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>6408790</u> JEM TOT	ENDING: <u>9.0</u> FT/IN OUT
ENDING: <u>72129.2</u> HRS	ENDING: <u>71098.4</u> HRS	BEGINNING: <u>6183430</u> JEM TOT	BEGINNING: <u>8.2</u> FT/IN OUT
BEGINNING: <u>72105.2</u> HRS	BEGINNING: <u>71074.4</u> HRS	TOTAL: <u>225.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2600520</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.8</u> KLB/HR	AVG. STEAM FLOW: <u>57.8</u> KLB/HR	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>191.8</u> TONS	APPROX REF PROC: <u>180.9</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>223.2</u> TONS	REFUSE PROCESSED: <u>231.3</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>33.8</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>89.5</u>	ENDING: <u>15</u> FT. OUT <u>45</u> IN OUT
TOTAL STEAM FLOW: <u>2726.7</u> KLB	GROSS REFUSE REC: <u>675.50</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>61</u> IN OUT
TOTAL REFUSE PR. <u>378.2</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>18.75</u>
	TOTAL REFUSE REC: <u>675.50</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>2,120.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>390427000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>5.51</u> TONS	
BEGINNING: <u>390138000</u> GAL		% OF REFUSE PROC: <u>1.46</u> %	
TOTAL USED: <u>289000</u> GAL	<u>153.65</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>86.8</u> %	UNIT 2 % MCR: <u>89.8</u> %	TG % MCR: <u>88.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.5</u>	GROSS KW/TON PR. <u>685.3</u>	
NET KWH/TON PR. <u>595.9</u>	LB LIME/TON PR.: <u>6.8</u>	TOT STM TO T/G: <u>2,714.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE January 21, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1318.5</u> KLB FEEDWATER USED: <u>1554.7</u> KLB	STEAM PRODUCED: <u>1315.8</u> KLB FEEDWATER USED: <u>1362.1</u> KLB	GENERATOR OUT: ENDING: <u>7611.0</u> WH TOT BEGINNING: <u>7602.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173487</u> CU FT ENDING: <u>173489</u> CU FT TOTAL USED: <u>2</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>236</u> KLB BLOWDOWN: <u>15.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>46</u> KLB BLOWDOWN: <u>3.4</u> %	UTILITY OUT: ENDING: <u>6620340</u> JEM TOT BEGINNING: <u>6408790</u> JEM TOT TOTAL: <u>211.6</u> MWH	PEBBLE LIME : ENDING: <u>7.9</u> FT/IN OUT BEGINNING: <u>9.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>72153.2</u> HRS BEGINNING: <u>72129.2</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>71122.4</u> HRS BEGINNING: <u>71098.4</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2600520</u> JEM TOT BEGINNING: <u>2600520</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>7.75</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>47.6</u> MWH KWH/TON: <u>118.2</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
AVG. STEAM FLOW: <u>54.9</u> KLB/HR	AVG. STEAM FLOW: <u>54.8</u> KLB/HR		CARBON INVENTORY: ENDING: <u>15</u> FT. OUT <u>16</u> IN OUT BEGINNING: <u>15</u> FT. OUT <u>45</u> IN OUT RECEIVED: <u>0.00</u> TONS
APPROX REF PROC: <u>207.0</u> TONS	APPROX REF PROC: <u>196.0</u> TONS		EOM OUT: <u>16.33</u>
REFUSE PROCESSED: <u>219.8</u> TONS	REFUSE PROCESSED: <u>219.3</u> TONS		
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2634.3</u> KLB TOTAL REFUSE PR. <u>403.0</u> TONS	GROSS REFUSE REC: <u>524.81</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>18.82</u> TONS ✓ TOTAL REFUSE REC: <u>505.99</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	
WELL WATER USE: ENDING: <u>390680000</u> GAL BEGINNING: <u>390427000</u> GAL TOTAL USED: <u>253000</u> GAL	EST PIT INVENTORY: <u>2,275.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>126.41</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>85.3</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>524.9</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>85.1</u> % LB STEAM/GROSS KW <u>10.2</u> LB LIME/TON PR.: <u>-8.6</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>643.2</u> TOT STM TO T/G: <u>2,587.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE January 22, 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1365.8</u> KLB FEEDWATER USED: <u>1809.3</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>243</u> KLB BLOWDOWN: <u>15.1</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72177.2</u> HRS BEGINNING: <u>72153.2</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>56.9</u> KLB/HR</p> <p>APPROX REF PROC: <u>221.0</u> TONS</p> <p>REFUSE PROCESSED: <u>227.6</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2744.9</u> KLB TOTAL REFUSE PR. <u>424.5</u> TONS</p> <p>WELL WATER USE: ENDING: <u>390991000</u> GAL BEGINNING: <u>390680000</u> GAL TOTAL USED: <u>311000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>88.4</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>525.1</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1379.1</u> KLB FEEDWATER USED: <u>1425.4</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>46</u> KLB BLOWDOWN: <u>3.3</u> %</p> <p>GRATE RUN TIME: ENDING: <u>71146.4</u> HRS BEGINNING: <u>71122.4</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>57.5</u> KLB/HR</p> <p>APPROX REF PROC: <u>202.0</u> TONS</p> <p>REFUSE PROCESSED: <u>229.8</u> TONS</p> <p>GROSS REFUSE REC: <u>614.33</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>614.33</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>2,859.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>152.65</u></p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>89.2</u> % LB STEAM/GROSS KW <u>9.5</u> LB LIME/TON PR.: <u>3.2</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>7621.0</u> WH TOT BEGINNING: <u>7611.0</u> WH TOT TOTAL: <u>288.0</u> MWH</p> <p>UTILITY OUT: ENDING: <u>6643230</u> JEM TOT BEGINNING: <u>6620340</u> JEM TOT TOTAL: <u>222.9</u> MWH</p> <p>UTILITY IN: ENDING: <u>2600520</u> JEM TOT BEGINNING: <u>2600520</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>65.1</u> MWH KWH/TON: <u>153.4</u></p> <p>MEDICAL WASTE : PROCESSED: <u>1.51</u> TONS % OF REFUSE PROC: <u>0.36</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>678.4</u> TOT STM TO T/G: <u>2,715.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173489</u> CU FT ENDING: <u>173489</u> CU FT TOTAL USED: <u>0</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>6.3</u> FT/IN OUT BEGINNING: <u>7.9</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>8.28</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>15</u> FT. OUT <u>34</u> IN OUT BEGINNING: <u>15</u> FT. OUT <u>16</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>17.83</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE January 23, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1336.5</u> KLB	STEAM PRODUCED: <u>1356.2</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1572.8</u> KLB	FEEDWATER USED: <u>1402.1</u> KLB	ENDING: <u>7629.0</u> WH TOT	BEGINNING: <u>173489</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7621.0</u> WH TOT	ENDING: <u>173489</u> CU FT
BLOWDOWN: <u>236</u> KLB	BLOWDOWN: <u>46</u> KLB	TOTAL: <u>230.4</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>15.0</u> %	BLOWDOWN: <u>3.3</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>7056120</u> JEM TOT	ENDING: <u>8.8</u> FT/IN OUT
ENDING: <u>72201.1</u> HRS	ENDING: <u>71170.4</u> HRS	BEGINNING: <u>6843230</u> JEM TOT	BEGINNING: <u>8.3</u> FT/IN OUT
BEGINNING: <u>72177.2</u> HRS	BEGINNING: <u>71146.4</u> HRS	TOTAL: <u>212.9</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>23.9</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>8.63</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.7</u> KLB/HR	AVG. STEAM FLOW: <u>56.5</u> KLB/HR	BEGINNING: <u>2600520</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>221.0</u> TONS	APPROX REF PROC: <u>215.0</u> TONS	TOTAL: <u>1.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>222.8</u> TONS	REFUSE PROCESSED: <u>226.0</u> TONS	GENERATOR RUN TIME: <u>23.5</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>18.5</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2692.7</u> KLB	GROSS REFUSE REC: <u>242.89</u> TONS	KWH/TON: <u>42.4</u>	ENDING: <u>15</u> FT. OUT <u>10</u> IN OUT
TOTAL REFUSE PR. <u>436.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>34</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
ENDING: <u>391280000</u> GAL	TOTAL REFUSE REC: <u>242.89</u> TONS ✓	MEDICAL WASTE:	EOM OUT: <u>15.83</u>
BEGINNING: <u>390991000</u> GAL	EST PIT INVENTORY: <u>1,634.0</u> TONS	PROCESSED: <u>0.00</u> TONS	
TOTAL USED: <u>289000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>97.9</u> %	
UNIT 1 % MCR: <u>86.5</u> %	UNIT 2 % MCR: <u>87.7</u> %	TG % MCR: <u>61.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>11.7</u>	GROSS KW/TON PR. <u>528.4</u>	
NET KWH/TON PR. <u>488.3</u>	LB LIME/TON PR.: <u>3.2</u>	TOT STM TO T/G: <u>2,660.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

Check valve problem with lube oil pump

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE January, 24, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1293.9</u> KLB FEEDWATER USED: <u>1523.9</u> KLB	STEAM PRODUCED: <u>1315.1</u> KLB FEEDWATER USED: <u>1354.4</u> KLB	GENERATOR OUT: ENDING: <u>7638.0</u> WH TOT BEGINNING: <u>7629.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173489</u> CU FT ENDING: <u>173489</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>230</u> KLB BLOWDOWN: <u>15.1</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>39</u> KLB BLOWDOWN: <u>2.9</u> %	UTILITY OUT: ENDING: <u>7268100</u> JEM TOT BEGINNING: <u>7056120</u> JEM TOT TOTAL: <u>212.0</u> MWH	PEBBLE LIME : ENDING: <u>8.9</u> FT/IN OUT BEGINNING: <u>8.8</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>72224.9</u> HRS BEGINNING: <u>72201.1</u> HRS TOTAL: <u>23.8</u> HRS	GRATE RUN TIME: ENDING: <u>71194.4</u> HRS BEGINNING: <u>71170.4</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>8.75</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>53.9</u> KLB/HR APPROX REF PROC: <u>215.0</u> TONS REFUSE PROCESSED: <u>215.7</u> TONS	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>54.8</u> KLB/HR APPROX REF PROC: <u>219.0</u> TONS REFUSE PROCESSED: <u>219.2</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>47.2</u> MWH KWH/TON: <u>108.8</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2609.0</u> KLB TOTAL REFUSE PR. <u>434.0</u> TONS	GROSS REFUSE REC: <u>0.00</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>0.00</u> TONS ✓		CARBON INVENTORY: ENDING: <u>14</u> FT. OUT <u>95</u> IN OUT BEGINNING: <u>15</u> FT. OUT <u>10</u> IN OUT RECEIVED: <u>0.00</u> TONS
WELL WATER USE: ENDING: <u>39158000</u> GAL BEGINNING: <u>39128000</u> GAL TOTAL USED: <u>278000</u> GAL	EST PIT INVENTORY: <u>1,050.0</u> TONS ✓ ASH HAULED: <u>0.00</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	EOM OUT: <u>21.92</u>
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>83.7</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>488.4</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>85.1</u> % LB STEAM/GROSS KW <u>10.1</u> LB LIME/TON PR.: <u>0.7</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>597.2</u> TOT STM TO T/G: <u>2,578.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 25, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1283.0</u> KLB FEEDWATER USED: <u>1511.0</u> KLB	STEAM PRODUCED: <u>1261.0</u> KLB FEEDWATER USED: <u>1297.0</u> KLB	GENERATOR OUT: ENDING: <u>7647.0</u> WH TOT BEGINNING: <u>7638.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173489</u> CU FT ENDING: <u>173491</u> CU FT TOTAL USED: <u>2</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>228</u> KLB BLOWDOWN: <u>15.1</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>36</u> KLB BLOWDOWN: <u>2.8</u> %	UTILITY OUT: ENDING: <u>7477210</u> JEM TOT BEGINNING: <u>7268100</u> JEM TOT TOTAL: <u>209.1</u> MWH	PEBBLE LIME : ENDING: <u>9.0</u> FT/IN OUT BEGINNING: <u>8.9</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>72248.9</u> HRS BEGINNING: <u>72224.9</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>71218.4</u> HRS BEGINNING: <u>71194.4</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>9.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>53.5</u> KLB/HR	AVG. STEAM FLOW: <u>52.5</u> KLB/HR	IN PLANT USE: <u>50.1</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>251.8</u> TONS	APPROX REF PROC: <u>216.3</u> TONS	KWH/TON: <u>118.1</u>	CARBON INVENTORY: ENDING: <u>14</u> FT. OUT <u>80</u> IN OUT BEGINNING: <u>14</u> FT. OUT <u>85</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>213.8</u> TONS	REFUSE PROCESSED: <u>210.2</u> TONS		EOM OUT: <u>20.67</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2544.0</u> KLB TOTAL REFUSE PR. <u>424.0</u> TONS	GROSS REFUSE REC: <u>683.03</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>683.03</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	
WELL WATER USE: ENDING: <u>391829000</u> GAL BEGINNING: <u>391558000</u> GAL TOTAL USED: <u>271000</u> GAL	EST PIT INVENTORY: <u>1,867.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>126.79</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>83.0</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>493.2</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>81.6</u> % LB STEAM/GROSS KW <u>9.8</u> LB LIME/TON PR.: <u>0.7</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>611.3</u> TOT STM TO T/G: <u>2,538.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 26, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1388.0</u> KLB	STEAM PRODUCED: <u>1263.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1634.5</u> KLB	FEEDWATER USED: <u>1295.5</u> KLB	ENDING: <u>7656.0</u> WH TOT	BEGINNING: <u>173491</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7647.0</u> WH TOT	ENDING: <u>173497</u> CU FT
BLOWDOWN: <u>247</u> KLB	BLOWDOWN: <u>33</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>6</u> CU FT
BLOWDOWN : <u>15.1</u> %	BLOWDOWN : <u>2.5</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>7693000</u> JEM TOT	ENDING: <u>9.9</u> FT/IN OUT
ENDING: <u>72272.9</u> HRS	ENDING: <u>71242.4</u> HRS	BEGINNING: <u>7477210</u> JEM TOT	BEGINNING: <u>9.0</u> FT/IN OUT
BEGINNING: <u>72248.9</u> HRS	BEGINNING: <u>71218.4</u> HRS	TOTAL: <u>215.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.75</u>
AVG. STEAM FLOW: <u>57.8</u> KLB/HR	AVG. STEAM FLOW: <u>52.6</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>231.3</u> TONS	APPROX REF PROC: <u>210.5</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>231.3</u> TONS	REFUSE PROCESSED: <u>210.5</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2651.0</u> KLB	GROSS REFUSE REC: <u>691.81</u> TONS	IN PLANT USE: <u>43.4</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>458.1</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>94.8</u>	ENDING: <u>14</u> FT. OUT <u>54</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>14</u> FT. OUT <u>80</u> IN OUT
ENDING: <u>392108000</u> GAL	TOTAL REFUSE REC: <u>691.81</u> TONS ✓	MEDICAL WASTE :	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>391829000</u> GAL	EST PIT INVENTORY: <u>2,217.0</u> TONS	PROCESSED: <u>16.27</u> TONS	EOM OUT: <u>18.50</u>
TOTAL USED: <u>279000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>3.55</u> %	
	<u>97.60</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>89.8</u> %	UNIT 2 % MCR: <u>81.7</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>565.9</u>	
NET KWH/TON PR. <u>471.1</u>	LB LIME/TON PR.: <u>6.2</u>	TOT STM TO T/G: <u>2,631.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 27, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1374.7</u> KLB	STEAM PRODUCED: <u>1263.2</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1610.6</u> KLB	FEEDWATER USED: <u>1297.2</u> KLB	ENDING: <u>7665.0</u> WH TOT	BEGINNING: <u>173497</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7656.0</u> WH TOT	ENDING: <u>173497</u> CU FT
BLOWDOWN: <u>236</u> KLB	BLOWDOWN: <u>34</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>14.6</u> %	BLOWDOWN: <u>2.6</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>7902030</u> JEM TOT	ENDING: <u>7.0</u> FT/IN OUT
ENDING: <u>72296.9</u> HRS	ENDING: <u>71266.4</u> HRS	BEGINNING: <u>7693000</u> JEM TOT	BEGINNING: <u>9.9</u> FT/IN OUT
BEGINNING: <u>72272.9</u> HRS	BEGINNING: <u>71242.4</u> HRS	TOTAL: <u>209.0</u> MWH	RECEIVED: <u>24.75</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>7.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>57.3</u> KLB/HR	AVG. STEAM FLOW: <u>52.8</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>228.0</u> TONS	APPROX REF PROC: <u>177.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>229.1</u> TONS	REFUSE PROCESSED: <u>210.5</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>50.2</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>119.0</u>	ENDING: <u>14</u> FT. OUT <u>32</u> IN OUT
TOTAL STEAM FLOW: <u>2637.9</u> KLB	GROSS REFUSE REC: <u>621.37</u> TONS		BEGINNING: <u>14</u> FT. OUT <u>54</u> IN OUT
TOTAL REFUSE PR. <u>421.8</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS <i>19.55</i>		
	TOTAL REFUSE REC: <u>621.37</u> TONS <i>601.82</i>		
WELL WATER USE:	EST PIT INVENTORY: <u>2,450.0</u> TONS	MEDICAL WASTE:	EOM OUT: <u>16.67</u>
ENDING: <u>392384000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>16.60</u> TONS	
BEGINNING: <u>392108000</u> GAL		% OF REFUSE PROC: <u>3.94</u> %	
TOTAL USED: <u>276000</u> GAL	<u>144.08</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>88.9</u> %	UNIT 2 % MCR: <u>81.7</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>614.8</u>	
NET KWH/TON PR. <u>495.8</u>	LB LIME/TON PR.: <u>95.8</u>	TOT STM TO T/G: <u>2,590.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 28, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1321.4</u> KLB	STEAM PRODUCED: <u>1464.3</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1546.7</u> KLB	FEEDWATER USED: <u>1495.1</u> KLB	ENDING: <u>7674.0</u> WH TOT	BEGINNING: <u>173497</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7865.0</u> WH TOT	ENDING: <u>173497</u> CU FT
BLOWDOWN: <u>225</u> KLB	BLOWDOWN: <u>31</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN : <u>14.6</u> %	BLOWDOWN : <u>2.1</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>8130990</u> JEM TOT	ENDING: <u>7.5</u> FT/IN OUT
ENDING: <u>72320.9</u> HRS	ENDING: <u>71290.4</u> HRS	BEGINNING: <u>7902030</u> JEM TOT	BEGINNING: <u>7.0</u> FT/IN OUT
BEGINNING: <u>72296.9</u> HRS	BEGINNING: <u>71266.4</u> HRS	TOTAL: <u>229.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>7.42</u>
AVG. STEAM FLOW: <u>55.1</u> KLB/HR	AVG. STEAM FLOW: <u>61.0</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>215.0</u> TONS	APPROX REF PROC: <u>208.0</u> TONS	BEGINNING: <u>2801500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>220.2</u> TONS	REFUSE PROCESSED: <u>244.1</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2785.7</u> KLB	GROSS REFUSE REC: <u>533.27</u> TONS	IN PLANT USE: <u>30.2</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>423.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>71.5</u>	ENDING: <u>14</u> FT. OUT <u>28</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>14</u> FT. OUT <u>32</u> IN OUT
ENDING: <u>392679000</u> GAL	TOTAL REFUSE REC: <u>533.27</u> TONS ✓	MEDICAL WASTE :	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>392384000</u> GAL	EST PIT INVENTORY: <u>2,509.0</u> TONS	PROCESSED: <u>0.00</u> TONS	EOM OUT: <u>16.33</u>
TOTAL USED: <u>295000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.00</u> %	
	<u>142.98</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.5</u> %	UNIT 2 % MCR: <u>94.7</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.7</u>	GROSS KW/TON PR. <u>612.8</u>	
NET KWH/TON PR. <u>541.3</u>	LB LIME/TON PR.: <u>3.7</u>	TOT STM TO T/G: <u>2,775.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 29, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1366.0</u> KLB FEEDWATER USED: <u>1593.1</u> KLB	STEAM PRODUCED: <u>1505.0</u> KLB FEEDWATER USED: <u>1534.1</u> KLB	GENERATOR OUT: ENDING: <u>7684.0</u> WH TOT BEGINNING: <u>7674.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173497</u> CU FT ENDING: <u>173497</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>227</u> KLB BLOWDOWN: <u>14.3</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>29</u> KLB BLOWDOWN: <u>1.9</u> %	UTILITY OUT: ENDING: <u>8369940</u> JEM TOT BEGINNING: <u>8130990</u> JEM TOT TOTAL: <u>239.0</u> MWH	PEBBLE LIME : ENDING: <u>8.0</u> FT/IN OUT BEGINNING: <u>7.5</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>72344.9</u> HRS BEGINNING: <u>72320.9</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>71314.4</u> HRS BEGINNING: <u>71290.4</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>8.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>56.9</u> KLB/HR	AVG. STEAM FLOW: <u>62.7</u> KLB/HR	IN PLANT USE: <u>49.1</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>210.0</u> TONS	APPROX REF PROC: <u>231.0</u> TONS	KWH/TON: <u>109.7</u>	CARBON INVENTORY: ENDING: <u>14</u> FT. OUT <u>23</u> IN OUT BEGINNING: <u>14</u> FT. OUT <u>28</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>227.7</u> TONS	REFUSE PROCESSED: <u>250.8</u> TONS		EOM OUT: <u>15.92</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2871.0</u> KLB TOTAL REFUSE PR. <u>447.1</u> TONS	GROSS REFUSE REC: <u>592.34</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>18.73</u> TONS ✓ TOTAL REFUSE REC: <u>573.61</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>6.05</u> TONS % OF REFUSE PROC: <u>1.35</u> %	
WELL WATER USE: ENDING: <u>392985000</u> GAL BEGINNING: <u>392679000</u> GAL TOTAL USED: <u>306000</u> GAL	EST PIT INVENTORY: <u>2,392.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>109.09</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>88.4</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>534.5</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>97.4</u> % LB STEAM/GROSS KW <u>10.0</u> LB LIME/TON PR.: <u>3.5</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>644.2</u> TOT STM TO T/G: <u>2,869.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 30, 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1427.0</u> KLB FEEDWATER USED: <u>1661.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>234</u> KLB BLOWDOWN : <u>14.1</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72368.9</u> HRS BEGINNING: <u>72344.9</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>59.5</u> KLB/HR</p> <p>APPROX REF PROC: <u>237.8</u> TONS</p> <p>REFUSE PROCESSED: <u>237.8</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2971.5</u> KLB TOTAL REFUSE PR. <u>509.9</u> TONS</p> <p>WELL WATER USE: ENDING: <u>393283000</u> GAL BEGINNING: <u>392985000</u> GAL TOTAL USED: <u>298000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>92.3</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>485.2</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1544.5</u> KLB FEEDWATER USED: <u>1574.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>30</u> KLB BLOWDOWN : <u>1.9</u> %</p> <p>GRATE RUN TIME: ENDING: <u>71338.4</u> HRS BEGINNING: <u>71314.4</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>64.4</u> KLB/HR</p> <p>APPROX REF PROC: <u>257.4</u> TONS</p> <p>REFUSE PROCESSED: <u>257.4</u> TONS</p> <p>GROSS REFUSE REC: <u>238.12</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS TOTAL REFUSE REC: <u>238.12</u> TONS</p> <p>EST PIT INVENTORY: <u>2,466.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>125.64</u></p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>99.9</u> % LB STEAM/GROSS KW <u>10.3</u> LB LIME/TON PR.: <u>6.2</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>7694.0</u> WH TOT BEGINNING: <u>7684.0</u> WH TOT TOTAL: <u>288.0</u> MWH</p> <p>UTILITY OUT: ENDING: <u>8617310</u> JEM TOT BEGINNING: <u>8369940</u> JEM TOT TOTAL: <u>247.4</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>40.6</u> MWH KWH/TON: <u>79.7</u></p> <p>MEDICAL WASTE : PROCESSED: <u>14.68</u> TONS % OF REFUSE PROC: <u>2.88</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>564.8</u> TOT STM TO T/G: <u>2,957.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173497</u> CU FT ENDING: <u>173524</u> CU FT TOTAL USED: <u>27</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>9.0</u> FT/IN OUT BEGINNING: <u>8.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>9.00</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS</p> <p>DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>14</u> FT. OUT <u>11</u> IN OUT BEGINNING: <u>14</u> FT. OUT <u>23</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>14.92</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JANUARY 31, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1448.4</u> KLB	STEAM PRODUCED: <u>1540.6</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1685.8</u> KLB	FEEDWATER USED: <u>1571.3</u> KLB	ENDING: <u>7705.0</u> WH TOT	BEGINNING: <u>173524</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7694.0</u> WH TOT	ENDING: <u>173539</u> CU FT
BLOWDOWN: <u>237</u> KLB	BLOWDOWN: <u>31</u> KLB	TOTAL: <u>316.8</u> MWH	TOTAL USED: <u>15</u> CU FT
BLOWDOWN: <u>14.1</u> %	BLOWDOWN: <u>2.0</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>8865450</u> JEM TOT	BEGINNING: <u>9.4</u> FT/IN OUT
ENDING: <u>72392.9</u> HRS	ENDING: <u>71362.4</u> HRS	BEGINNING: <u>8617310</u> JEM TOT	BEGINNING: <u>9.0</u> FT/IN OUT
BEGINNING: <u>72368.9</u> HRS	BEGINNING: <u>71338.4</u> HRS	TOTAL: <u>248.1</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.33</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>60.4</u> KLB/HR	AVG. STEAM FLOW: <u>64.2</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>237.0</u> TONS	APPROX REF PROC: <u>238.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>241.4</u> TONS	REFUSE PROCESSED: <u>256.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>68.7</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>141.8</u>	ENDING: <u>14</u> FT. OUT <u>0</u> IN OUT
TOTAL STEAM FLOW: <u>2989.0</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS		BEGINNING: <u>14</u> FT. OUT <u>11</u> IN OUT
TOTAL REFUSE PR. <u>484.3</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>14.00</u>
	TOTAL REFUSE REC: <u>0.00</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>1,692.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>393596000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	PROCESSED: <u>9.32</u> TONS	
BEGINNING: <u>393283000</u> GAL		% OF REFUSE PROC: <u>1.92</u> %	
TOTAL USED: <u>313000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>93.7</u> %	UNIT 2 % MCR: <u>99.7</u> %	TG % MCR: <u>84.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.4</u>	GROSS KW/TON PR. <u>654.1</u>	
NET KWH/TON PR. <u>512.3</u>	LB LIME/TON PR.: <u>2.6</u>	TOT STM TO T/G: <u>2,974.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 01, 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1394.1</u> KLB FEEDWATER USED: <u>1625.5</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>231</u> KLB BLOWDOWN: <u>14.2</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72416.9</u> HRS BEGINNING: <u>72392.9</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>58.1</u> KLB/HR</p> <p>APPROX REF PROC: <u>222.0</u> TONS</p> <p>REFUSE PROCESSED: <u>232.4</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2877.6</u> KLB TOTAL REFUSE PR. <u>471.6</u> TONS</p> <p>WELL WATER USE: ENDING: <u>393910000</u> GAL BEGINNING: <u>393596000</u> GAL TOTAL USED: <u>314000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>90.2</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>512.3</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1483.5</u> KLB FEEDWATER USED: <u>1511.3</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>28</u> KLB BLOWDOWN: <u>1.8</u> %</p> <p>GRATE RUN TIME: ENDING: <u>71386.4</u> HRS BEGINNING: <u>71362.4</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>61.8</u> KLB/HR</p> <p>APPROX REF PROC: <u>239.0</u> TONS</p> <p>REFUSE PROCESSED: <u>247.3</u> TONS</p> <p>GROSS REFUSE REC: <u>641.81</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>641.81</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>2,023.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>176.09</u></p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>96.0</u> % LB STEAM/GROSS KW <u>10.0</u> LB LIME/TON PR.: <u>4.0</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>7715.0</u> WH TOT BEGINNING: <u>7705.0</u> WH TOT TOTAL: <u>288.0</u> MWH</p> <p>UTILITY OUT: ENDING: <u>9107060</u> JEM TOT BEGINNING: <u>8865450</u> JEM TOT TOTAL: <u>241.6</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>46.4</u> MWH KWH/TON: <u>98.4</u></p> <p>MEDICAL WASTE : PROCESSED: <u>10.61</u> TONS % OF REFUSE PROC: <u>2.25</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>610.7</u> TOT STM TO T/G: <u>2,882.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173539</u> CU FT ENDING: <u>173540</u> CU FT TOTAL USED: <u>1</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>10.0</u> FT/IN OUT BEGINNING: <u>9.4</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>10.00</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS</p> <p>DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>13</u> FT. OUT <u>98</u> IN OUT BEGINNING: <u>14</u> FT. OUT <u>0</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>21.17</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 02, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1429.0</u> KLB FEEDWATER USED: <u>1664.0</u> KLB	STEAM PRODUCED: <u>1559.0</u> KLB FEEDWATER USED: <u>1587.5</u> KLB	GENERATOR OUT: ENDING: <u>7725.0</u> WH TOT BEGINNING: <u>7715.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173540</u> CU FT ENDING: <u>173540</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>235</u> KLB BLOWDOWN: <u>14.1</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>29</u> KLB BLOWDOWN: <u>1.8</u> %	UTILITY OUT: ENDING: <u>9359370</u> JEM TOT BEGINNING: <u>9107060</u> JEM TOT TOTAL: <u>252.3</u> MWH	PEBBLE LIME : ENDING: <u>10.3</u> FT/IN OUT BEGINNING: <u>10.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>72440.9</u> HRS BEGINNING: <u>72416.9</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>71410.4</u> HRS BEGINNING: <u>71386.4</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>10.25</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>59.5</u> KLB/HR APPROX REF PROC: <u>226.0</u> TONS	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>65.0</u> KLB/HR APPROX REF PROC: <u>211.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>35.7</u> MWH KWH/TON: <u>79.8</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
REFUSE PROCESSED: <u>238.2</u> TONS	REFUSE PROCESSED: <u>259.8</u> TONS		CARBON INVENTORY: ENDING: <u>13</u> FT. OUT <u>88</u> IN OUT BEGINNING: <u>13</u> FT. OUT <u>98</u> IN OUT RECEIVED: <u>0.00</u> TONS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			EOM OUT: <u>20.33</u>
TOTAL STEAM FLOW: <u>2988.0</u> KLB TOTAL REFUSE PR. <u>447.4</u> TONS	GROSS REFUSE REC: <u>658.30</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>658.30</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>10.38</u> TONS % OF REFUSE PROC: <u>2.32</u> %	
WELL WATER USE: ENDING: <u>394263000</u> GAL BEGINNING: <u>393910000</u> GAL TOTAL USED: <u>353000</u> GAL	EST PIT INVENTORY: <u>2,295.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>151.12</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>92.5</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>584.0</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>100.9</u> % LB STEAM/GROSS KW <u>10.4</u> LB LIME/TON PR.: <u>2.1</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>643.7</u> TOT STM TO T/G: <u>2,887.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 03, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1416.5</u> KLB	STEAM PRODUCED: <u>1505.2</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1647.9</u> KLB	FEEDWATER USED: <u>1535.5</u> KLB	ENDING: <u>7735.0</u> WH TOT	BEGINNING: <u>173540</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7725.0</u> WH TOT	ENDING: <u>173543</u> CU FT
BLOWDOWN: <u>231</u> KLB	BLOWDOWN: <u>30</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>3</u> CU FT
BLOWDOWN: <u>14.0</u> %	BLOWDOWN: <u>2.0</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>9603660</u> JEM TOT	ENDING: <u>0.0</u> FT/IN OUT
ENDING: <u>72464.9</u> HRS	ENDING: <u>71434.4</u> HRS	BEGINNING: <u>9359370</u> JEM TOT	BEGINNING: <u>10.3</u> FT/IN OUT
BEGINNING: <u>72440.9</u> HRS	BEGINNING: <u>71410.4</u> HRS	TOTAL: <u>244.3</u> MWH	RECEIVED: <u>24.67</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>0.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.0</u> KLB/HR	AVG. STEAM FLOW: <u>62.7</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>219.0</u> TONS	APPROX REF PROC: <u>228.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>236.1</u> TONS	REFUSE PROCESSED: <u>250.9</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>43.7</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>95.5</u>	ENDING: <u>13</u> FT. OUT <u>78</u> IN OUT
TOTAL STEAM FLOW: <u>2921.7</u> KLB	GROSS REFUSE REC: <u>596.92</u> TONS		BEGINNING: <u>13</u> FT. OUT <u>88</u> IN OUT
TOTAL REFUSE PR. <u>457.9</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>19.50</u>
	TOTAL REFUSE REC: <u>596.92</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>2,354.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>394612000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>10.85</u> TONS	
BEGINNING: <u>394263000</u> GAL	<u>25.35</u>	% OF REFUSE PROC: <u>2.37</u> %	
TOTAL USED: <u>349000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>91.6</u> %	UNIT 2 % MCR: <u>97.4</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.1</u>	GROSS KW/TON PR. <u>629.0</u>	
NET KWH/TON PR. <u>533.6</u>	LB LIME/TON PR.: <u>38.0</u>	TOT STM TO T/G: <u>2,910.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 04, 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1385.0</u> KLB FEEDWATER USED: <u>1612.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>227</u> KLB BLOWDOWN: <u>14.1</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72488.9</u> HRS BEGINNING: <u>72464.9</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>57.7</u> KLB/HR APPROX REF PROC: <u>225.0</u> TONS REFUSE PROCESSED: <u>230.8</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2835.0</u> KLB TOTAL REFUSE PR. <u>444.3</u> TONS</p> <p>WELL WATER USE: ENDING: <u>394947000</u> GAL BEGINNING: <u>394612000</u> GAL TOTAL USED: <u>335000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>89.6</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>527.0</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1450.0</u> KLB FEEDWATER USED: <u>1482.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>32</u> KLB BLOWDOWN: <u>2.2</u> %</p> <p>GRATE RUN TIME: ENDING: <u>71458.4</u> HRS BEGINNING: <u>71434.4</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>60.4</u> KLB/HR APPROX REF PROC: <u>212.0</u> TONS REFUSE PROCESSED: <u>241.7</u> TONS</p> <p>GROSS REFUSE REC: <u>531.49</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>17.52</u> TONS ✓ TOTAL REFUSE REC: <u>513.97</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>2,628.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>102.55</u></p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>93.8</u> % LB STEAM/GROSS KW <u>9.8</u> LB LIME/TON PR.: <u>53.7</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>7745.0</u> WH TOT BEGINNING: <u>7735.0</u> WH TOT TOTAL: <u>288.0</u> MWH</p> <p>UTILITY OUT: ENDING: <u>9837790</u> JEM TOT BEGINNING: <u>9603660</u> JEM TOT TOTAL: <u>234.1</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>53.9</u> MWH KWH/TON: <u>121.2</u></p> <p>MEDICAL WASTE : PROCESSED: <u>7.30</u> TONS % OF REFUSE PROC: <u>1.64</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>648.2</u> TOT STM TO T/G: <u>2,812.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173543</u> CU FT ENDING: <u>173590</u> CU FT TOTAL USED: <u>47</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>7.6</u> FT/IN OUT BEGINNING: <u>0.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>7.50</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>13</u> FT. OUT <u>78</u> IN OUT BEGINNING: <u>13</u> FT. OUT <u>78</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>19.50</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 05, 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1383.0</u> KLB FEEDWATER USED: <u>1612.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>229</u> KLB BLOWDOWN : <u>14.2</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72512.8</u> HRS BEGINNING: <u>72488.9</u> HRS TOTAL: <u>23.9</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>57.6</u> KLB/HR</p> <p>APPROX REF PROC: <u>226.6</u> TONS</p> <p>REFUSE PROCESSED: <u>230.5</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2830.0</u> KLB TOTAL REFUSE PR. <u>473.8</u> TONS</p> <p>WELL WATER USE: ENDING: <u>395274000</u> GAL BEGINNING: <u>394947000</u> GAL TOTAL USED: <u>327000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>89.5</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>499.0</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1447.0</u> KLB FEEDWATER USED: <u>1478.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>31</u> KLB BLOWDOWN : <u>2.1</u> %</p> <p>GRATE RUN TIME: ENDING: <u>71482.4</u> HRS BEGINNING: <u>71458.4</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>60.3</u> KLB/HR</p> <p>APPROX REF PROC: <u>238.4</u> TONS</p> <p>REFUSE PROCESSED: <u>241.2</u> TONS</p> <p>GROSS REFUSE REC: <u>611.76</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>611.76</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>2,626.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>208.08</u></p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>93.8</u> % LB STEAM/GROSS KW <u>9.8</u> LB LIME/TON PR.: <u>2.7</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>7755.0</u> WH TOT BEGINNING: <u>7745.0</u> WH TOT TOTAL: <u>288.0</u> MWH</p> <p>UTILITY OUT: ENDING: <u>10074200</u> JEM TOT BEGINNING: <u>9837790</u> JEM TOT TOTAL: <u>236.4</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>51.6</u> MWH KWH/TON: <u>108.9</u></p> <p>MEDICAL WASTE : PROCESSED: <u>8.77</u> TONS % OF REFUSE PROC: <u>1.85</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>607.9</u> TOT STM TO T/G: <u>2,809.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173590</u> CU FT ENDING: <u>173591</u> CU FT TOTAL USED: <u>1</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>8.0</u> FT/IN OUT BEGINNING: <u>7.6</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>8.00</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS</p> <p>DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>13</u> FT. OUT <u>1</u> IN OUT BEGINNING: <u>13</u> FT. OUT <u>78</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>13.08</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 06, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1357.0</u> KLB	STEAM PRODUCED: <u>1483.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1814.0</u> KLB	FEEDWATER USED: <u>1493.0</u> KLB	ENDING: <u>7765.0</u> WH TOT	BEGINNING: <u>173591</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7755.0</u> WH TOT	ENDING: <u>173597</u> CU FT
BLOWDOWN: <u>257</u> KLB	BLOWDOWN: <u>30</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>6</u> CU FT
BLOWDOWN %: <u>15.9</u> %	BLOWDOWN %: <u>2.0</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>309550</u> JEM TOT	ENDING: <u>8.3</u> FT/IN OUT
ENDING: <u>72536.6</u> HRS	ENDING: <u>71506.3</u> HRS	BEGINNING: <u>74200</u> JEM TOT	BEGINNING: <u>8.0</u> FT/IN OUT
BEGINNING: <u>72512.8</u> HRS	BEGINNING: <u>71482.4</u> HRS	TOTAL: <u>235.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>23.8</u> HRS	TOTAL: <u>23.9</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>8.25</u>
AVG. STEAM FLOW: <u>56.5</u> KLB/HR	AVG. STEAM FLOW: <u>61.0</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>228.0</u> TONS	APPROX REF PROC: <u>245.0</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>226.2</u> TONS	REFUSE PROCESSED: <u>243.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2820.0</u> KLB	GROSS REFUSE REC: <u>236.07</u> TONS	IN PLANT USE: <u>52.7</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>482.1</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>109.2</u>	ENDING: <u>13</u> FT. OUT <u>1</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>21.74</u> TONS ✓		BEGINNING: <u>13</u> FT. OUT <u>1</u> IN OUT
ENDING: <u>395574000</u> GAL	TOTAL REFUSE REC: <u>214.33</u> TONS ✓	MEDICAL WASTE:	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>395274000</u> GAL	EST PIT INVENTORY: <u>2,392.0</u> TONS	PROCESSED: <u>12.13</u> TONS	EOM OUT: <u>13.08</u>
TOTAL USED: <u>300000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.52</u> %	
	<u>125.14</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>87.8</u> %	UNIT 2 % MCR: <u>94.7</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.8</u>	GROSS KW/TON PR. <u>597.3</u>	
NET KWH/TON PR. <u>488.1</u>	LB LIME/TON PR.: <u>2.0</u>	TOT STM TO T/G: <u>2,823.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 07, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1419.0</u> KLB	STEAM PRODUCED: <u>1481.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1666.0</u> KLB	FEEDWATER USED: <u>1511.0</u> KLB	ENDING: <u>7774.0</u> WH TOT	BEGINNING: <u>173597</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7765.0</u> WH TOT	ENDING: <u>173597</u> CU FT
BLOWDOWN: <u>247</u> KLB	BLOWDOWN: <u>30</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN : <u>14.8</u> %	BLOWDOWN : <u>2.0</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>551950</u> JEM TOT	ENDING: <u>8.7</u> FT/IN OUT
ENDING: <u>72560.5</u> HRS	ENDING: <u>71530.2</u> HRS	BEGINNING: <u>309550</u> JEM TOT	BEGINNING: <u>8.3</u> FT/IN OUT
BEGINNING: <u>72536.6</u> HRS	BEGINNING: <u>71506.3</u> HRS	TOTAL: <u>242.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>23.9</u> HRS	TOTAL: <u>23.9</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>8.58</u>
AVG. STEAM FLOW: <u>59.1</u> KLB/HR	AVG. STEAM FLOW: <u>61.7</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>244.0</u> TONS	APPROX REF PROC: <u>241.0</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>236.5</u> TONS	REFUSE PROCESSED: <u>246.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2900.0</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS	IN PLANT USE: <u>16.8</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>486.6</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>34.5</u>	ENDING: <u>12</u> FT. OUT <u>68</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓	MEDICAL WASTE :	BEGINNING: <u>13</u> FT. OUT <u>1</u> IN OUT
ENDING: <u>395878000</u> GAL	TOTAL REFUSE REC: <u>0.00</u> TONS ✓	PROCESSED: <u>3.22</u> TONS	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>395574000</u> GAL	EST PIT INVENTORY: <u>1,809.0</u> TONS	% OF REFUSE PROC: <u>0.66</u> %	EOM OUT: <u>17.50</u>
TOTAL USED: <u>304000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>91.8</u> %	UNIT 2 % MCR: <u>95.8</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>11.2</u>	GROSS KW/TON PR. <u>532.7</u>	
NET KWH/TON PR. <u>488.2</u>	LB LIME/TON PR.: <u>2.6</u>	TOT STM TO T/G: <u>2,807.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 08 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1397.8</u> KLB FEEDWATER USED: <u>1873.2</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>275</u> KLB BLOWDOWN : <u>16.5</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72584.5</u> HRS BEGINNING: <u>72560.5</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>58.2</u> KLB/HR APPROX REF PROC: <u>214.6</u> TONS REFUSE PROCESSED: <u>233.0</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2928.9</u> KLB TOTAL REFUSE PR. <u>453.6</u> TONS</p> <p>WELL WATER USE: ENDING: <u>396191000</u> GAL BEGINNING: <u>395878000</u> GAL TOTAL USED: <u>313000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>90.4</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>550.1</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1531.1</u> KLB FEEDWATER USED: <u>1558.6</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>28</u> KLB BLOWDOWN : <u>1.8</u> %</p> <p>GRATE RUN TIME: ENDING: <u>71554.2</u> HRS BEGINNING: <u>71530.2</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>63.8</u> KLB/HR APPROX REF PROC: <u>230.8</u> TONS REFUSE PROCESSED: <u>255.2</u> TONS</p> <p>GROSS REFUSE REC: <u>703.60</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>703.60</u> TONS <u>703.68</u></p> <p>EST PIT INVENTORY: <u>2,159.0</u> TONS ASH HAULED: <u>0.00</u> TONS ✓</p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>99.1</u> % LB STEAM/GROSS KW <u>10.2</u> LB LIME/TON PR.: <u>0.0</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>7784.0</u> WH TOT BEGINNING: <u>7774.0</u> WH TOT TOTAL: <u>288.0</u> MWH</p> <p>UTILITY OUT: ENDING: <u>801480</u> JEM TOT BEGINNING: <u>551950</u> JEM TOT TOTAL: <u>249.5</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>38.5</u> MWH KWH/TON: <u>84.9</u></p> <p>MEDICAL WASTE : PROCESSED: <u>8.38</u> TONS % OF REFUSE PROC: <u>1.85</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>634.9</u> TOT STM TO T/G: <u>2,980.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173597</u> CU FT ENDING: <u>173597</u> CU FT TOTAL USED: <u>0</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>8.7</u> FT/IN OUT BEGINNING: <u>8.7</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>8.58</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS</p> <p>DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>12</u> FT. OUT <u>75</u> IN OUT BEGINNING: <u>12</u> FT. OUT <u>68</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>18.25</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 09, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1376.0</u> KLB	STEAM PRODUCED: <u>1552.4</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1610.0</u> KLB	FEEDWATER USED: <u>1581.9</u> KLB	ENDING: <u>7794.0</u> WH TOT	BEGINNING: <u>173597</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7784.0</u> WH TOT	ENDING: <u>173642</u> CU FT
BLOWDOWN: <u>234</u> KLB	BLOWDOWN: <u>30</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>45</u> CU FT
BLOWDOWN : <u>14.5</u> %	BLOWDOWN : <u>1.9</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1044630</u> JEM TOT	ENDING: <u>9.6</u> FT/IN OUT
ENDING: <u>72608.5</u> HRS	ENDING: <u>71578.2</u> HRS	BEGINNING: <u>801460</u> JEM TOT	BEGINNING: <u>8.7</u> FT/IN OUT
BEGINNING: <u>72584.5</u> HRS	BEGINNING: <u>71554.2</u> HRS	TOTAL: <u>243.2</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.50</u>
AVG. STEAM FLOW: <u>57.3</u> KLB/HR	AVG. STEAM FLOW: <u>64.7</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>235.8</u> TONS	APPROX REF PROC: <u>253.8</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>229.3</u> TONS	REFUSE PROCESSED: <u>258.7</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2928.4</u> KLB	GROSS REFUSE REC: <u>686.67</u> TONS	IN PLANT USE: <u>44.8</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>494.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>90.7</u>	ENDING: <u>12</u> FT. OUT <u>44</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>12</u> FT. OUT <u>75</u> IN OUT
ENDING: <u>396507000</u> GAL	TOTAL REFUSE REC: <u>686.67</u> TONS ✓	MEDICAL WASTE :	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>396191000</u> GAL	EST PIT INVENTORY: <u>2,392.0</u> TONS	PROCESSED: <u>5.98</u> TONS	EOM OUT: <u>15.67</u>
TOTAL USED: <u>316000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.21</u> %	
	<u>255.49</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>89.0</u> %	UNIT 2 % MCR: <u>100.4</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>582.9</u>	
NET KWH/TON PR. <u>492.2</u>	LB LIME/TON PR.: <u>5.7</u>	TOT STM TO T/G: <u>2,920.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 10, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1352.5</u> KLB	STEAM PRODUCED: <u>1534.6</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1589.9</u> KLB	FEEDWATER USED: <u>1565.4</u> KLB	ENDING: <u>7804.0</u> WH TOT	BEGINNING: <u>173642</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7794.0</u> WH TOT	ENDING: <u>173655</u> CU FT
BLOWDOWN: <u>237</u> KLB	BLOWDOWN: <u>31</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>13</u> CU FT
BLOWDOWN: <u>14.9</u> %	BLOWDOWN: <u>2.0</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1285850</u> JEM TOT	ENDING: <u>4.4</u> FT/IN OUT
ENDING: <u>72632.5</u> HRS	ENDING: <u>71602.2</u> HRS	BEGINNING: <u>1044630</u> JEM TOT	BEGINNING: <u>9.6</u> FT/IN OUT
BEGINNING: <u>72608.5</u> HRS	BEGINNING: <u>71578.2</u> HRS	TOTAL: <u>241.2</u> MWH	RECEIVED: <u>25.01</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>4.33</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>56.4</u> KLB/HR	AVG. STEAM FLOW: <u>63.9</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>203.4</u> TONS	APPROX REF PROC: <u>211.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>225.4</u> TONS	REFUSE PROCESSED: <u>255.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>46.8</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2887.1</u> KLB	GROSS REFUSE REC: <u>635.24</u> TONS	KWH/TON: <u>111.1</u>	ENDING: <u>12</u> FT. OUT <u>18</u> IN OUT
TOTAL REFUSE PR. <u>421.2</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>12</u> FT. OUT <u>44</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>23.77</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
ENDING: <u>396788000</u> GAL	TOTAL REFUSE REC: <u>611.47</u> TONS ✓	MEDICAL WASTE :	EOM OUT: <u>13.50</u>
BEGINNING: <u>396507000</u> GAL	EST PIT INVENTORY: <u>2,781.0</u> TONS	PROCESSED: <u>5.98</u> TONS	
TOTAL USED: <u>281000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.42</u> %	
	<u>120.04</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>87.5</u> %	UNIT 2 % MCR: <u>99.3</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.0</u>	GROSS KW/TON PR. <u>683.8</u>	
NET KWH/TON PR. <u>572.7</u>	LB LIME/TON PR.: <u>80.0</u>	TOT STM TO T/G: <u>2,877.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 11, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1367.0</u> KLB	STEAM PRODUCED: <u>1541.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1595.0</u> KLB	FEEDWATER USED: <u>1571.0</u> KLB	ENDING: <u>7815.0</u> WH TOT	BEGINNING: <u>173655</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7804.0</u> WH TOT	ENDING: <u>173871</u> CU FT
BLOWDOWN: <u>228</u> KLB	BLOWDOWN: <u>30</u> KLB	TOTAL: <u>316.8</u> MWH	TOTAL USED: <u>16</u> CU FT
BLOWDOWN %: <u>14.3</u> %	BLOWDOWN %: <u>1.9</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1528460</u> JEM TOT	ENDING: <u>6.4</u> FT/IN OUT
ENDING: <u>72656.5</u> HRS	ENDING: <u>71626.2</u> HRS	BEGINNING: <u>1285850</u> JEM TOT	BEGINNING: <u>4.4</u> FT/IN OUT
BEGINNING: <u>72832.5</u> HRS	BEGINNING: <u>71602.2</u> HRS	TOTAL: <u>242.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>6.33</u>
AVG. STEAM FLOW: <u>57.0</u> KLB/HR	AVG. STEAM FLOW: <u>64.2</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	
APPROX REF PROC: <u>214.5</u> TONS	APPROX REF PROC: <u>238.1</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	CARBON USAGE:
REFUSE PROCESSED: <u>227.8</u> TONS	REFUSE PROCESSED: <u>256.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #1: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	USAGE UNIT #2: <u>269</u> LBS
		IN PLANT USE: <u>74.2</u> MWH	DAILY TOTAL: <u>538</u> LBS
		KWH/TON: <u>161.3</u>	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2908.0</u> KLB	GROSS REFUSE REC: <u>497.00</u> TONS		ENDING: <u>12</u> FT. OUT <u>0</u> IN OUT
TOTAL REFUSE PR. <u>460.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>12</u> FT. OUT <u>18</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>497.00</u> TONS ✓		EOM OUT: <u>12.00</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,509.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>397081000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>7.39</u> TONS	
BEGINNING: <u>398788000</u> GAL		% OF REFUSE PROC: <u>1.81</u> %	
TOTAL USED: <u>273000</u> GAL	<u>133,49</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>88.4</u> %	UNIT 2 % MCR: <u>99.7</u> %	TG % MCR: <u>84.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.2</u>	GROSS KW/TON PR. <u>688.7</u>	
NET KWH/TON PR. <u>527.4</u>	LB LIME/TON PR.: <u>13.7</u>	TOT STM TO T/G: <u>2,893.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 12, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1287.0</u> KLB	STEAM PRODUCED: <u>1521.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1499.0</u> KLB	FEEDWATER USED: <u>1548.0</u> KLB	ENDING: <u>7824.0</u> WH TOT	BEGINNING: <u>173671</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7815.0</u> WH TOT	ENDING: <u>173671</u> CU FT
BLOWDOWN: <u>212</u> KLB	BLOWDOWN: <u>27</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>14.1</u> %	BLOWDOWN: <u>1.7</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1761560</u> JEM TOT	ENDING: <u>6.6</u> FT/IN OUT
ENDING: <u>72680.5</u> HRS	ENDING: <u>71650.2</u> HRS	BEGINNING: <u>1528460</u> JEM TOT	BEGINNING: <u>6.4</u> FT/IN OUT
BEGINNING: <u>72656.5</u> HRS	BEGINNING: <u>71626.2</u> HRS	TOTAL: <u>233.1</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>6.50</u>
AVG. STEAM FLOW: <u>53.6</u> KLB/HR	AVG. STEAM FLOW: <u>63.4</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>203.2</u> TONS	APPROX REF PROC: <u>236.6</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>214.5</u> TONS	REFUSE PROCESSED: <u>253.5</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2808.0</u> KLB	GROSS REFUSE REC: <u>592.68</u> TONS	IN PLANT USE: <u>26.1</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>445.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>58.6</u>	ENDING: <u>11</u> FT. OUT <u>95</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>12</u> FT. OUT <u>0</u> IN OUT
ENDING: <u>397328000</u> GAL	TOTAL REFUSE REC: <u>592.68</u> TONS ✓	MEDICAL WASTE:	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>397061000</u> GAL	EST PIT INVENTORY: <u>2,625.0</u> TONS	PROCESSED: <u>5.70</u> TONS	EOM OUT: <u>18.92</u>
TOTAL USED: <u>267000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.28</u> %	
	<u>117,86</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>83.3</u> %	UNIT 2 % MCR: <u>98.4</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.8</u>	GROSS KW/TON PR. <u>581.8</u>	
NET KWH/TON PR. <u>523.2</u>	LB LIME/TON PR.: <u>1.4</u>	TOT STM TO T/G: <u>2,790.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 13 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1339.1</u> KLB	STEAM PRODUCED: <u>1513.9</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1559.1</u> KLB	FEEDWATER USED: <u>1542.3</u> KLB	ENDING: <u>7834.0</u> WH TOT	BEGINNING: <u>173671</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7824.0</u> WH TOT	ENDING: <u>173671</u> CU FT
BLOWDOWN: <u>220</u> KLB	BLOWDOWN: <u>28</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>14.1</u> %	BLOWDOWN: <u>1.8</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1998910</u> JEM TOT	ENDING: <u>6.0</u> FT/IN OUT
ENDING: <u>72704.5</u> HRS	ENDING: <u>71674.2</u> HRS	BEGINNING: <u>1761560</u> JEM TOT	BEGINNING: <u>6.6</u> FT/IN OUT
BEGINNING: <u>72680.5</u> HRS	BEGINNING: <u>71650.2</u> HRS	TOTAL: <u>237.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>6.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.8</u> KLB/HR	AVG. STEAM FLOW: <u>63.1</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>220.9</u> TONS	APPROX REF PROC: <u>230.4</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>223.2</u> TONS	REFUSE PROCESSED: <u>252.3</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>50.7</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>111.4</u>	ENDING: <u>11</u> FT. OUT <u>52</u> IN OUT
TOTAL STEAM FLOW: <u>2853.0</u> KLB	GROSS REFUSE REC: <u>253.70</u> TONS		BEGINNING: <u>12</u> FT. OUT <u>0</u> IN OUT
TOTAL REFUSE PR. <u>454.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS		EOM OUT: <u>15.33</u>
	TOTAL REFUSE REC: <u>253.70</u> TONS <i>253.72</i>		
WELL WATER USE:	EST PIT INVENTORY: <u>2,295.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>397586000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>3.35</u> TONS	
BEGINNING: <u>397328000</u> GAL		% OF REFUSE PROC: <u>0.74</u> %	
TOTAL USED: <u>258000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>86.6</u> %	UNIT 2 % MCR: <u>97.9</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.9</u>	GROSS KW/TON PR. <u>633.5</u>	
NET KWH/TON PR. <u>522.0</u>	LB LIME/TON PR.: <u>-4.1</u>	TOT STM TO T/G: <u>2,780.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 14 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1380.4</u> KLB FEEDWATER USED: <u>1606.6</u> KLB	STEAM PRODUCED: <u>1543.8</u> KLB FEEDWATER USED: <u>1572.4</u> KLB	GENERATOR OUT: ENDING: <u>7844.0</u> WH TOT BEGINNING: <u>7834.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173671</u> CU FT ENDING: <u>173671</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>226</u> KLB BLOWDOWN: <u>14.1</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>29</u> KLB BLOWDOWN: <u>1.8</u> %	UTILITY OUT: ENDING: <u>2244770</u> JEM TOT BEGINNING: <u>1998910</u> JEM TOT TOTAL: <u>245.9</u> MWH	PEBBLE LIME: ENDING: <u>6.9</u> FT/IN OUT BEGINNING: <u>6.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>72728.5</u> HRS BEGINNING: <u>72704.5</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>71698.2</u> HRS BEGINNING: <u>71674.2</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>6.75</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>57.5</u> KLB/HR APPROX REF PROC: <u>217.8</u> TONS	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>64.3</u> KLB/HR APPROX REF PROC: <u>231.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>42.1</u> MWH KWH/TON: <u>93.7</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
REFUSE PROCESSED: <u>230.1</u> TONS	REFUSE PROCESSED: <u>257.3</u> TONS	NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB	CARBON INVENTORY: ENDING: <u>12</u> FT. OUT <u>8</u> IN OUT BEGINNING: <u>11</u> FT. OUT <u>52</u> IN OUT RECEIVED: <u>0.00</u> TONS
TOTAL STEAM FLOW: <u>2924.2</u> KLB TOTAL REFUSE PR. <u>449.6</u> TONS	GROSS REFUSE REC: <u>0.00</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>0.00</u> TONS ✓	WELL WATER USE: ENDING: <u>397841000</u> GAL BEGINNING: <u>397586000</u> GAL TOTAL USED: <u>255000</u> GAL	EOM OUT: <u>12.67</u>
EST PIT INVENTORY: <u>1,945.0</u> TONS ASH HAULED: <u>0.00</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>89.3</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>546.8</u>	
UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>99.9</u> % LB STEAM/GROSS KW <u>10.2</u> LB LIME/TON PR.: <u>6.3</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>78.4</u> % GROSS KW/TON PR. <u>640.5</u> TOT STM TO T/G: <u>2,918.0</u>		

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 15 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1292.2</u> KLB	STEAM PRODUCED: <u>1522.8</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1502.5</u> KLB	FEEDWATER USED: <u>1549.3</u> KLB	ENDING: <u>7854.0</u> WH TOT	BEGINNING: <u>173671</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7844.0</u> WH TOT	ENDING: <u>173671</u> CU FT
BLOWDOWN: <u>210</u> KLB	BLOWDOWN: <u>27</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN %: <u>14.0</u> %	BLOWDOWN %: <u>1.7</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2479290</u> JEM TOT	ENDING: <u>6.1</u> FT/IN OUT
ENDING: <u>72752.5</u> HRS	ENDING: <u>71722.2</u> HRS	BEGINNING: <u>2244770</u> JEM TOT	BEGINNING: <u>6.0</u> FT/IN OUT
BEGINNING: <u>72728.5</u> HRS	BEGINNING: <u>71698.2</u> HRS	TOTAL: <u>234.5</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>6.09</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>53.8</u> KLB/HR	AVG. STEAM FLOW: <u>63.5</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>289</u> LBS
APPROX REF PROC: <u>182.0</u> TONS	APPROX REF PROC: <u>221.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>215.4</u> TONS	REFUSE PROCESSED: <u>253.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>53.5</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>128.2</u>	ENDING: <u>12</u> FT. OUT <u>9</u> IN OUT
TOTAL STEAM FLOW: <u>2815.0</u> KLB	GROSS REFUSE REC: <u>627.92</u> TONS		BEGINNING: <u>12</u> FT. OUT <u>18</u> IN OUT
TOTAL REFUSE PR. <u>417.2</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓	MEDICAL WASTE:	EOM OUT: <u>12.75</u>
ENDING: <u>398092000</u> GAL	TOTAL REFUSE REC: <u>627.92</u> TONS <u>624.60</u>	PROCESSED: <u>4.24</u> TONS	
BEGINNING: <u>397841000</u> GAL	EST PIT INVENTORY: <u>2,140.0</u> TONS	% OF REFUSE PROC: <u>1.02</u> %	
TOTAL USED: <u>251000</u> GAL	ASH HAULED: <u>0.00</u> TONS		
	<u>134.14</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>83.6</u> %	UNIT 2 % MCR: <u>98.5</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.8</u>	GROSS KW/TON PR. <u>690.3</u>	
NET KWH/TON PR. <u>562.1</u>	LB LIME/TON PR.: <u>0.8</u>	TOT STM TO T/G: <u>2,813.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 16 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1413.5</u> KLB FEEDWATER USED: <u>1644.3</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>231</u> KLB BLOWDOWN : <u>14.0</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72776.5</u> HRS BEGINNING: <u>72752.5</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>58.9</u> KLB/HR APPROX REF PROC: <u>214.7</u> TONS REFUSE PROCESSED: <u>235.6</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2941.9</u> KLB TOTAL REFUSE PR. <u>429.1</u> TONS</p> <p>WELL WATER USE: ENDING: <u>398398000</u> GAL BEGINNING: <u>398092000</u> GAL TOTAL USED: <u>306000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>91.5</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>574.3</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1528.4</u> KLB FEEDWATER USED: <u>1556.7</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>28</u> KLB BLOWDOWN : <u>1.8</u> %</p> <p>GRATE RUN TIME: ENDING: <u>71746.2</u> HRS BEGINNING: <u>71722.2</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>63.7</u> KLB/HR APPROX REF PROC: <u>214.4</u> TONS REFUSE PROCESSED: <u>254.7</u> TONS</p> <p>GROSS REFUSE REC: <u>655.33</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>22.72</u> TONS TOTAL REFUSE REC: <u>632.61</u> TONS</p> <p>EST PIT INVENTORY: <u>2,431.0</u> TONS ASH HAULED: <u>0.00</u> TONS</p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>98.9</u> % LB STEAM/GROSS KW <u>10.2</u> LB LIME/TON PR.: <u>13.9</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>7864.0</u> WH TOT BEGINNING: <u>7854.0</u> WH TOT TOTAL: <u>288.0</u> MWH</p> <p>UTILITY OUT: ENDING: <u>2725730</u> JEM TOT BEGINNING: <u>2479290</u> JEM TOT TOTAL: <u>246.4</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>41.6</u> MWH KWH/TON: <u>96.9</u></p> <p>MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>671.2</u> TOT STM TO T/G: <u>2,945.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173671</u> CU FT ENDING: <u>173730</u> CU FT TOTAL USED: <u>59</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>8.0</u> FT/IN OUT BEGINNING: <u>6.1</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>8.00</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>11</u> FT. OUT <u>72</u> IN OUT BEGINNING: <u>12</u> FT. OUT <u>9</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>17.00</u></p>
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NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB

247.87

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 17 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1476.9</u> KLB	STEAM PRODUCED: <u>1537.1</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1718.5</u> KLB	FEEDWATER USED: <u>1564.6</u> KLB	ENDING: <u>7875.0</u> WH TOT	BEGINNING: <u>173730</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7864.0</u> WH TOT	ENDING: <u>173730</u> CU FT
BLOWDOWN: <u>242</u> KLB	BLOWDOWN: <u>28</u> KLB	TOTAL: <u>316.8</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>14.1</u> %	BLOWDOWN: <u>1.8</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2983730</u> JEM TOT	ENDING: <u>4.9</u> FT/IN OUT
ENDING: <u>72800.5</u> HRS	ENDING: <u>71770.2</u> HRS	BEGINNING: <u>2725730</u> JEM TOT	BEGINNING: <u>8.0</u> FT/IN OUT
BEGINNING: <u>72776.5</u> HRS	BEGINNING: <u>71746.2</u> HRS	TOTAL: <u>258.0</u> MWH	RECEIVED: <u>23.41</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>4.75</u>
AVG. STEAM FLOW: <u>61.5</u> KLB/HR	AVG. STEAM FLOW: <u>64.0</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>223.4</u> TONS	APPROX REF PROC: <u>219.5</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>246.2</u> TONS	REFUSE PROCESSED: <u>256.2</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>3014.0</u> KLB	GROSS REFUSE REC: <u>509.31</u> TONS	IN PLANT USE: <u>58.8</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>460.8</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>127.6</u>	ENDING: <u>11</u> FT. OUT <u>48</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓	MEDICAL WASTE:	BEGINNING: <u>11</u> FT. OUT <u>72</u> IN OUT
ENDING: <u>398713000</u> GAL	TOTAL REFUSE REC: <u>509.31</u> TONS ✓	PROCESSED: <u>17.85</u> TONS	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>398398000</u> GAL	EST PIT INVENTORY: <u>2,431.0</u> TONS	% OF REFUSE PROC: <u>3.87</u> %	EOM OUT: <u>14.83</u>
TOTAL USED: <u>315000</u> GAL	ASH HAULED: <u>0.00</u> TONS		
	<u>94.97</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>95.6</u> %	UNIT 2 % MCR: <u>99.5</u> %	TG % MCR: <u>84.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.5</u>	GROSS KW/TON PR. <u>687.6</u>	
NET KWH/TON PR. <u>580.0</u>	LB LIME/TON PR.: <u>80.5</u>	TOT STM TO T/G: <u>3,047.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE February 18, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1499.0</u> KLB	STEAM PRODUCED: <u>1482.7</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1745.1</u> KLB	FEEDWATER USED: <u>1513.9</u> KLB	ENDING: <u>7885.0</u> WH TOT	BEGINNING: <u>173730</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7875.0</u> WH TOT	ENDING: <u>173730</u> CU FT
BLOWDOWN: <u>246</u> KLB	BLOWDOWN: <u>31</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>14.1</u> %	BLOWDOWN: <u>2.1</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3236860</u> JEM TOT	ENDING: <u>5.0</u> FT/IN OUT
ENDING: <u>72824.5</u> HRS	ENDING: <u>71794.2</u> HRS	BEGINNING: <u>2983730</u> JEM TOT	BEGINNING: <u>4.9</u> FT/IN OUT
BEGINNING: <u>72800.5</u> HRS	BEGINNING: <u>71770.2</u> HRS	TOTAL: <u>253.1</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>5.00</u>
AVG. STEAM FLOW: <u>62.5</u> KLB/HR	AVG. STEAM FLOW: <u>61.8</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>250.1</u> TONS	APPROX REF PROC: <u>193.2</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>249.8</u> TONS	REFUSE PROCESSED: <u>247.1</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2981.6</u> KLB	GROSS REFUSE REC: <u>508.18</u> TONS	IN PLANT USE: <u>34.9</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>456.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>76.4</u>	ENDING: <u>21</u> FT. OUT <u>68</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>11</u> FT. OUT <u>48</u> IN OUT
ENDING: <u>399020000</u> GAL	TOTAL REFUSE REC: <u>508.18</u> TONS ✓	MEDICAL WASTE:	RECEIVED: <u>20.10</u> TONS
BEGINNING: <u>398713000</u> GAL	EST PIT INVENTORY: <u>2,528.0</u> TONS	PROCESSED: <u>13.25</u> TONS	EOM OUT: <u>26.67</u>
TOTAL USED: <u>307000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.90</u> %	
	<u>60.56</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>97.0</u> %	UNIT 2 % MCR: <u>95.9</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.4</u>	GROSS KW/TON PR. <u>630.8</u>	
NET KWH/TON PR. <u>554.5</u>	LB LIME/TON PR.: <u>0.7</u>	TOT STM TO T/G: <u>3,016.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE February 19, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1506.7</u> KLB	STEAM PRODUCED: <u>1483.9</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1750.9</u> KLB	FEEDWATER USED: <u>1511.9</u> KLB	ENDING: <u>7895.0</u> WH TOT	BEGINNING: <u>173730</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7885.0</u> WH TOT	ENDING: <u>173733</u> CU FT
BLOWDOWN: <u>244</u> KLB	BLOWDOWN: <u>28</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>3</u> CU FT
BLOWDOWN: <u>13.9</u> %	BLOWDOWN: <u>1.9</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3490690</u> JEM TOT	ENDING: <u>5.1</u> FT/IN OUT
ENDING: <u>72848.5</u> HRS	ENDING: <u>71818.2</u> HRS	BEGINNING: <u>3236860</u> JEM TOT	BEGINNING: <u>5.0</u> FT/IN OUT
BEGINNING: <u>72824.5</u> HRS	BEGINNING: <u>71794.2</u> HRS	TOTAL: <u>253.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>5.08</u>
AVG. STEAM FLOW: <u>62.8</u> KLB/HR	AVG. STEAM FLOW: <u>61.8</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>253.3</u> TONS	APPROX REF PROC: <u>232.2</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>251.1</u> TONS	REFUSE PROCESSED: <u>247.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2990.6</u> KLB	GROSS REFUSE REC: <u>612.46</u> TONS	IN PLANT USE: <u>34.2</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>492.2</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>69.4</u>	ENDING: <u>21</u> FT. OUT <u>31</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>23.59</u> TONS ✓		BEGINNING: <u>21</u> FT. OUT <u>68</u> IN OUT
ENDING: <u>399345000</u> GAL	TOTAL REFUSE REC: <u>588.87</u> TONS ✓	MEDICAL WASTE:	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>399020000</u> GAL	EST PIT INVENTORY: <u>2,567.0</u> TONS	PROCESSED: <u>6.76</u> TONS	EOM OUT: <u>23.58</u>
TOTAL USED: <u>325000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.37</u> %	
	<u>272.31</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>97.5</u> %	UNIT 2 % MCR: <u>96.0</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.4</u>	GROSS KW/TON PR. <u>585.1</u>	
NET KWH/TON PR. <u>515.7</u>	LB LIME/TON PR.: <u>0.8</u>	TOT STM TO T/G: <u>3,002.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE February 20, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1448.0</u> KLB	STEAM PRODUCED: <u>1469.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1683.6</u> KLB	FEEDWATER USED: <u>1488.5</u> KLB	ENDING: <u>7906.0</u> WH TOT	BEGINNING: <u>173733</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7895.0</u> WH TOT	ENDING: <u>173733</u> CU FT
BLOWDOWN: <u>238</u> KLB	BLOWDOWN: <u>30</u> KLB	TOTAL: <u>316.8</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>14.1</u> %	BLOWDOWN: <u>2.0</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3735470</u> JEM TOT	ENDING: <u>5.3</u> FT/IN OUT
ENDING: <u>72872.5</u> HRS	ENDING: <u>71842.2</u> HRS	BEGINNING: <u>3490690</u> JEM TOT	BEGINNING: <u>5.1</u> FT/IN OUT
BEGINNING: <u>72848.5</u> HRS	BEGINNING: <u>71818.2</u> HRS	TOTAL: <u>244.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>5.25</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>60.3</u> KLB/HR	AVG. STEAM FLOW: <u>61.2</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>188.1</u> TONS	APPROX REF PROC: <u>183.9</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>241.0</u> TONS	REFUSE PROCESSED: <u>244.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>72.0</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>189.1</u>	ENDING: <u>21</u> FT. OUT <u>122</u> IN OUT
TOTAL STEAM FLOW: <u>2915.0</u> KLB	GROSS REFUSE REC: <u>281.63</u> TONS		BEGINNING: <u>21</u> FT. OUT <u>31</u> IN OUT
TOTAL REFUSE PR. <u>380.8</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
<u>494.6</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>31.17</u>
WELL WATER USE:	TOTAL REFUSE REC: <u>281.63</u> TONS ✓	MEDICAL WASTE:	
ENDING: <u>399653000</u> GAL	EST PIT INVENTORY: <u>2,188.0</u> TONS	PROCESSED: <u>8.86</u> TONS	
BEGINNING: <u>399345000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.33</u> %	
TOTAL USED: <u>308000</u> GAL	<u>225.13</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>93.6</u> %	UNIT 2 % MCR: <u>95.0</u> %	TG % MCR: <u>84.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.2</u>	GROSS KW/TON PR. <u>831.9</u>	
NET KWH/TON PR. <u>642.8</u>	LB LIME/TON PR.: <u>1.6</u>	TOT STM TO T/G: <u>2,902.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE February 21, 1989

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1441.0</u> KLB FEEDWATER USED: <u>1685.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>244</u> KLB BLOWDOWN : <u>14.5</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72896.5</u> HRS BEGINNING: <u>72872.5</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>60.0</u> KLB/HR APPROX REF PROC: <u>201.2</u> TONS REFUSE PROCESSED: <u>240.2</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2917.0</u> KLB TOTAL REFUSE PR. <u>392.3</u> TONS</p> <p>WELL WATER USE: ENDING: <u>399945000</u> GAL BEGINNING: <u>399653000</u> GAL TOTAL USED: <u>292000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>93.2</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>619.4</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1476.0</u> KLB FEEDWATER USED: <u>1507.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>31</u> KLB BLOWDOWN : <u>2.1</u> %</p> <p>GRATE RUN TIME: ENDING: <u>71866.2</u> HRS BEGINNING: <u>71842.2</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>61.5</u> KLB/HR APPROX REF PROC: <u>184.5</u> TONS REFUSE PROCESSED: <u>246.0</u> TONS</p> <p>GROSS REFUSE REC: <u>0.00</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>0.00</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>1,879.0</u> TONS ASH HAULED: <u>0.00</u> TONS ✓</p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>95.5</u> % LB STEAM/GROSS KW <u>11.3</u> LB LIME/TON PR.: <u>2.4</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>7915.0</u> WH TOT BEGINNING: <u>7906.0</u> WH TOT TOTAL: <u>259.2</u> MWH</p> <p>UTILITY OUT: ENDING: <u>3978460</u> JEM TOT BEGINNING: <u>3735470</u> JEM TOT TOTAL: <u>243.0</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>16.2</u> MWH KWH/TON: <u>41.3</u></p> <p>MEDICAL WASTE : PROCESSED: <u>6.82</u> TONS % OF REFUSE PROC: <u>1.89</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>680.7</u> TOT STM TO T/G: <u>2,915.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173733</u> CU FT ENDING: <u>173733</u> CU FT TOTAL USED: <u>0</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>5.6</u> FT/IN OUT BEGINNING: <u>5.3</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>5.50</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>21</u> FT. OUT <u>2</u> IN OUT BEGINNING: <u>21</u> FT. OUT <u>12</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>21.17</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 22, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1427.0</u> KLB FEEDWATER USED: <u>1662.0</u> KLB	STEAM PRODUCED: <u>1459.0</u> KLB FEEDWATER USED: <u>1489.0</u> KLB	GENERATOR OUT: ENDING: <u>7925.0</u> WH TOT BEGINNING: <u>7915.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173733</u> CU FT ENDING: <u>173761</u> CU FT TOTAL USED: <u>28</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>235</u> KLB BLOWDOWN : <u>14.1</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>30</u> KLB BLOWDOWN : <u>2.0</u> %	UTILITY OUT: ENDING: <u>4220400</u> JEM TOT BEGINNING: <u>3978460</u> JEM TOT TOTAL: <u>241.9</u> MWH	PEBBLE LIME : ENDING: <u>5.8</u> FT/IN OUT BEGINNING: <u>5.8</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>72920.5</u> HRS BEGINNING: <u>72896.5</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>71890.2</u> HRS BEGINNING: <u>71868.2</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>5.67</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>59.5</u> KLB/HR	AVG. STEAM FLOW: <u>60.8</u> KLB/HR	IN PLANT USE: <u>46.1</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>215.0</u> TONS	APPROX REF PROC: <u>191.0</u> TONS	KWH/TON: <u>111.5</u>	CARBON INVENTORY: ENDING: <u>20</u> FT. OUT <u>95</u> IN OUT BEGINNING: <u>21</u> FT. OUT <u>2</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>237.8</u> TONS	REFUSE PROCESSED: <u>243.2</u> TONS		EOM OUT: <u>27.92</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2886.0</u> KLB TOTAL REFUSE PR. <u>413.3</u> TONS <i>458.25</i>	GROSS REFUSE REC: <u>653.78</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS TOTAL REFUSE REC: <u>653.78</u> TONS <i>669.03</i>	MEDICAL WASTE : PROCESSED: <u>7.25</u> TONS % OF REFUSE PROC: <u>1.75</u> %	
WELL WATER USE: ENDING: <u>400238000</u> GAL BEGINNING: <u>399945000</u> GAL TOTAL USED: <u>283000</u> GAL	EST PIT INVENTORY: <u>2,392.0</u> TONS ASH HAULED: <u>0.00</u> TONS <i>129.15</i>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>92.3</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>585.5</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>94.4</u> % LB STEAM/GROSS KW <u>10.0</u> LB LIME/TON PR.: <u>1.5</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>696.9</u> TOT STM TO T/G: <u>2,875.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 23, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1393.0</u> KLB	STEAM PRODUCED: <u>1457.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>O/S</u> KLB	FEEDWATER USED: <u>1466.0</u> KLB	ENDING: <u>7935.0</u> WH TOT	BEGINNING: <u>173781</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7925.0</u> WH TOT	ENDING: <u>173791</u> CU FT
BLOWDOWN: <u>-1393</u> KLB	BLOWDOWN: <u>29</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>30</u> CU FT
BLOWDOWN: <u>ERR</u> %	BLOWDOWN: <u>2.0</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4480810</u> JEM TOT	ENDING: <u>6.9</u> FT/IN OUT
ENDING: <u>72944.5</u> HRS	ENDING: <u>71914.2</u> HRS	BEGINNING: <u>4220400</u> JEM TOT	BEGINNING: <u>5.8</u> FT/IN OUT
BEGINNING: <u>72920.5</u> HRS	BEGINNING: <u>71890.2</u> HRS	TOTAL: <u>240.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>6.75</u>
AVG. STEAM FLOW: <u>58.0</u> KLB/HR	AVG. STEAM FLOW: <u>60.7</u> KLB/HR	ENDING: <u>2801500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>203.0</u> TONS	APPROX REF PROC: <u>187.0</u> TONS	BEGINNING: <u>2801500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>232.2</u> TONS	REFUSE PROCESSED: <u>242.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
		IN PLANT USE: <u>47.6</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>117.6</u>	ENDING: <u>20</u> FT. OUT <u>88</u> IN OUT
TOTAL STEAM FLOW: <u>2850.0</u> KLB	GROSS REFUSE REC: <u>617.25</u> TONS		BEGINNING: <u>20</u> FT. OUT <u>95</u> IN OUT
TOTAL REFUSE PR. <u>404.8</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
<u>489.7</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>27.33</u>
WELL WATER USE:	TOTAL REFUSE REC: <u>617.25</u> TONS <u>617.02</u>	MEDICAL WASTE :	
ENDING: <u>400539000</u> GAL	EST PIT INVENTORY: <u>2,334.0</u> TONS	PROCESSED: <u>14.78</u> TONS	
BEGINNING: <u>400238000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>3.85</u> %	
TOTAL USED: <u>301000</u> GAL	<u>140.08</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>90.1</u> %	UNIT 2 % MCR: <u>94.3</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>8.9</u>	GROSS KW/TON PR. <u>711.5</u>	
NET KWH/TON PR. <u>593.9</u>	LB LIME/TON PR.: <u>8.5</u>	TOT STM TO T/G: <u>2,850.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 24, 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1347.0</u> KLB FEEDWATER USED: <u>O/S</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>-1347</u> KLB BLOWDOWN: <u>ERR</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72968.5</u> HRS BEGINNING: <u>72944.5</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>56.1</u> KLB/HR</p> <p>APPROX REF PROC: <u>192.0</u> TONS</p> <p>REFUSE PROCESSED: <u>224.5</u> TONS</p> <p>NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB</p> <p>TOTAL STEAM FLOW: <u>2801.0</u> KLB TOTAL REFUSE PR. <u>407.8</u> TONS <u>476.58</u></p> <p>WELL WATER USE: ENDING: <u>400824000</u> GAL BEGINNING: <u>400539000</u> GAL TOTAL USED: <u>285000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>87.2</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>579.3</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1454.0</u> KLB FEEDWATER USED: <u>1484.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>30</u> KLB BLOWDOWN: <u>2.0</u> %</p> <p>GRATE RUN TIME: ENDING: <u>71938.2</u> HRS BEGINNING: <u>71914.2</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>60.6</u> KLB/HR</p> <p>APPROX REF PROC: <u>206.0</u> TONS</p> <p>REFUSE PROCESSED: <u>242.3</u> TONS</p> <p>GROSS REFUSE REC: <u>601.79</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>601.79</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>2,723.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>101.45</u></p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>94.1</u> % LB STEAM/GROSS KW <u>9.7</u> LB LIME/TON PR.: <u>99.6</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>7945.0</u> WH TOT BEGINNING: <u>7935.0</u> WH TOT TOTAL: <u>288.0</u> MWH</p> <p>UTILITY OUT: ENDING: <u>4697020</u> JEM TOT BEGINNING: <u>4460810</u> JEM TOT TOTAL: <u>236.2</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>51.6</u> MWH KWH/TON: <u>127.0</u></p> <p>MEDICAL WASTE : PROCESSED: <u>9.78</u> TONS % OF REFUSE PROC: <u>2.40</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>706.3</u> TOT STM TO T/G: <u>2,825.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173791</u> CU FT ENDING: <u>173791</u> CU FT TOTAL USED: <u>0</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>4.4</u> FT/IN OUT BEGINNING: <u>6.9</u> FT/IN OUT RECEIVED: <u>24.24</u> TONS</p> <p>EOM OUT: <u>4.33</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>20</u> FT. OUT <u>76</u> IN OUT BEGINNING: <u>20</u> FT. OUT <u>88</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>26.33</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 25 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1419.5</u> KLB	STEAM PRODUCED: <u>1465.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1468.0</u> KLB	FEEDWATER USED: <u>1496.6</u> KLB	ENDING: <u>7955.0</u> WH TOT	BEGINNING: <u>173791</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>7945.0</u> WH TOT	ENDING: <u>173795</u> CU FT
BLOWDOWN: <u>49</u> KLB	BLOWDOWN: <u>32</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>4</u> CU FT
BLOWDOWN : <u>3.3</u> %	BLOWDOWN : <u>2.1</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4938380</u> JEM TOT	ENDING: <u>4.6</u> FT/IN OUT
ENDING: <u>72992.5</u> HRS	ENDING: <u>71962.2</u> HRS	BEGINNING: <u>4697020</u> JEM TOT	BEGINNING: <u>4.4</u> FT/IN OUT
BEGINNING: <u>72988.5</u> HRS	BEGINNING: <u>71938.2</u> HRS	TOTAL: <u>241.3</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>4.50</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.1</u> KLB/HR	AVG. STEAM FLOW: <u>61.0</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>212.0</u> TONS	APPROX REF PROC: <u>212.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>236.6</u> TONS	REFUSE PROCESSED: <u>244.2</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>48.7</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2884.5</u> KLB	GROSS REFUSE REC: <u>598.10</u> TONS ✓	KWH/TON: <u>108.7</u>	ENDING: <u>20</u> FT. OUT <u>59</u> IN OUT
TOTAL REFUSE PR. <u>429.3</u> TONS	NON PROCESSED: <u>0.00</u> TONS ✓		BEGINNING <u>20</u> FT. OUT <u>76</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
ENDING: <u>401119000</u> GAL	TOTAL REFUSE REC: <u>598.10</u> TONS ✓	MEDICAL WASTE :	EOM OUT: <u>24.92</u>
BEGINNING: <u>400824000</u> GAL	EST PIT INVENTORY: <u>2,509.0</u> TONS	PROCESSED: <u>5.27</u> TONS	
TOTAL USED: <u>295000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.23</u> %	
	<u>146.32</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>91.8</u> %	UNIT 2 % MCR: <u>94.8</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.0</u>	GROSS KW/TON PR. <u>670.9</u>	
NET KWH/TON PR. <u>582.2</u>	LB LIME/TON PR.: <u>1.5</u>	TOT STM TO T/G: <u>2,880.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 26, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1449.8</u> KLB FEEDWATER USED: <u>1497.2</u> KLB	STEAM PRODUCED: <u>1468.6</u> KLB FEEDWATER USED: <u>1499.0</u> KLB	GENERATOR OUT: ENDING: <u>7965.0</u> WH TOT BEGINNING: <u>7955.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173795</u> CU FT ENDING: <u>173795</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>47</u> KLB BLOWDOWN : <u>3.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>30</u> KLB BLOWDOWN : <u>2.0</u> %	UTILITY OUT: ENDING: <u>5182490</u> JEM TOT BEGINNING: <u>4936360</u> JEM TOT TOTAL: <u>244.1</u> MWH	PEBBLE LIME : ENDING: <u>5.0</u> FT/IN OUT BEGINNING: <u>4.6</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>73016.5</u> HRS BEGINNING: <u>72992.5</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>71986.2</u> HRS BEGINNING: <u>71962.2</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>5.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>60.4</u> KLB/HR	AVG. STEAM FLOW: <u>61.2</u> KLB/HR	IN PLANT USE: <u>43.9</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>225.0</u> TONS	APPROX REF PROC: <u>235.0</u> TONS	KWH/TON: <u>93.4</u>	CARBON INVENTORY: ENDING: <u>20</u> FT. OUT <u>55</u> IN OUT BEGINNING: <u>20</u> FT. OUT <u>59</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>241.6</u> TONS	REFUSE PROCESSED: <u>244.8</u> TONS		EOM OUT: <u>24.58</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2918.4</u> KLB TOTAL REFUSE PR. <u>469.5</u> TONS	GROSS REFUSE REC: <u>584.23</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>584.23</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>9.49</u> TONS % OF REFUSE PROC: <u>2.02</u> %	
WELL WATER USE: ENDING: <u>401420000</u> GAL BEGINNING: <u>401119000</u> GAL TOTAL USED: <u>301000</u> GAL	EST PIT INVENTORY: <u>2,859.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>98.55</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>93.8</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>520.0</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>95.0</u> % LB STEAM/GROSS KW <u>10.1</u> LB LIME/TON PR.: <u>2.7</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>613.4</u> TOT STM TO T/G: <u>2,910.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE FEBRUARY 27, 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1457.0</u> KLB FEEDWATER USED: <u>1504.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>47</u> KLB BLOWDOWN : <u>3.1</u> %</p> <p>GRATE RUN TIME: ENDING: <u>73040.5</u> HRS BEGINNING: <u>73016.5</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>60.7</u> KLB/HR APPROX REF PROC: <u>219.0</u> TONS REFUSE PROCESSED: <u>242.8</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2982.0</u> KLB TOTAL REFUSE PR. <u>442.8</u> TONS</p> <p>WELL WATER USE: ENDING: <u>401731000</u> GAL BEGINNING: <u>401420000</u> GAL TOTAL USED: <u>311000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>94.3</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>574.1</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1525.0</u> KLB FEEDWATER USED: <u>1555.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>30</u> KLB BLOWDOWN : <u>1.9</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72010.2</u> HRS BEGINNING: <u>71986.2</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>63.5</u> KLB/HR APPROX REF PROC: <u>222.0</u> TONS REFUSE PROCESSED: <u>254.2</u> TONS</p> <p>GROSS REFUSE REC: <u>265.84</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>19.55</u> TONS TOTAL REFUSE REC: <u>246.29</u> TONS</p> <p>EST PIT INVENTORY: <u>2,548.0</u> TONS ASH HAULED: <u>0.00</u> TONS</p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>98.7</u> % LB STEAM/GROSS KW <u>9.4</u> LB LIME/TON PR.: <u>2.1</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>7976.0</u> WH TOT BEGINNING: <u>7965.0</u> WH TOT TOTAL: <u>316.8</u> MWH</p> <p>UTILITY OUT: ENDING: <u>5436700</u> JEM TOT BEGINNING: <u>5182490</u> JEM TOT TOTAL: <u>254.2</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>62.8</u> MWH KWH/TON: <u>141.4</u></p> <p>MEDICAL WASTE : PROCESSED: <u>1.77</u> TONS % OF REFUSE PROC: <u>0.40</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>84.1</u> % GROSS KW/TON PR. <u>715.5</u> TOT STM TO T/G: <u>2,910.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173795</u> CU FT ENDING: <u>173799</u> CU FT TOTAL USED: <u>4</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>5.3</u> FT/IN OUT BEGINNING: <u>5.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>5.25</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS</p> <p>DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>20</u> FT. OUT <u>45</u> IN OUT BEGINNING: <u>20</u> FT. OUT <u>55</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>23.75</u></p>
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127.38

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE FEBRUARY 28, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1448.0</u> KLB FEEDWATER USED: <u>1496.0</u> KLB	STEAM PRODUCED: <u>1516.5</u> KLB FEEDWATER USED: <u>1546.5</u> KLB	GENERATOR OUT: ENDING: <u>7986.0</u> WH TOT BEGINNING: <u>7976.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173799</u> CU FT ENDING: <u>173800</u> CU FT TOTAL USED: <u>1</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>48</u> KLB BLOWDOWN: <u>3.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>30</u> KLB BLOWDOWN: <u>1.9</u> %	UTILITY OUT: ENDING: <u>5688330</u> JEM TOT BEGINNING: <u>5436700</u> JEM TOT TOTAL: <u>251.6</u> MWH	PEBBLE LIME : ENDING: <u>5.7</u> FT/IN OUT BEGINNING: <u>5.3</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>73064.5</u> HRS BEGINNING: <u>73040.5</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>72034.2</u> HRS BEGINNING: <u>72010.2</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>5.58</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>60.3</u> KLB/HR	AVG. STEAM FLOW: <u>63.2</u> KLB/HR	IN PLANT USE: <u>36.4</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>239.9</u> TONS	APPROX REF PROC: <u>227.0</u> TONS	KWH/TON: <u>77.9</u>	CARBON INVENTORY: ENDING: <u>20</u> FT. OUT <u>30</u> IN OUT BEGINNING: <u>20</u> FT. OUT <u>45</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>241.3</u> TONS	REFUSE PROCESSED: <u>252.8</u> TONS		EOM OUT: <u>22.50</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2964.5</u> KLB TOTAL REFUSE PR. <u>486.9</u> TONS	GROSS REFUSE REC: <u>0.00</u> TONS ✓ NON PROCESSED: <u>0.00</u> TONS ✓ FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>0.00</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	
WELL WATER USE: ENDING: <u>402043000</u> GAL BEGINNING: <u>401731000</u> GAL TOTAL USED: <u>312000</u> GAL	EST PIT INVENTORY: <u>1,890.0</u> TONS ASH HAULED: <u>0.00</u> TONS ✓		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>93.7</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>538.9</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>98.1</u> % LB STEAM/GROSS KW <u>10.3</u> LB LIME/TON PR.: <u>2.7</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>616.8</u> TOT STM TO T/G: <u>2,962.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 01, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1411.0</u> KLB FEEDWATER USED: <u>1457.0</u> KLB	STEAM PRODUCED: <u>1413.0</u> KLB FEEDWATER USED: <u>1442.0</u> KLB	GENERATOR OUT: ENDING: <u>7996.0</u> WH TOT BEGINNING: <u>7986.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173800</u> CU FT ENDING: <u>173800</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>46</u> KLB BLOWDOWN: <u>3.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>29</u> KLB BLOWDOWN: <u>2.0</u> %	UTILITY OUT: ENDING: <u>5923760</u> JEM TOT BEGINNING: <u>5688330</u> JEM TOT TOTAL: <u>235.4</u> MWH	PEBBLE LIME: ENDING: <u>6.5</u> FT/IN OUT BEGINNING: <u>5.7</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>73088.5</u> HRS BEGINNING: <u>73064.5</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>72058.2</u> HRS BEGINNING: <u>72034.2</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>6.42</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>58.8</u> KLB/HR APPROX REF PROC: <u>208.0</u> TONS	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>58.9</u> KLB/HR APPROX REF PROC: <u>225.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>52.6</u> MWH KWH/TON: <u>118.5</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
REFUSE PROCESSED: <u>235.2</u> TONS	REFUSE PROCESSED: <u>235.5</u> TONS	NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB	CARBON INVENTORY: ENDING: <u>20</u> FT. OUT <u>10</u> IN OUT BEGINNING: <u>20</u> FT. OUT <u>30</u> IN OUT RECEIVED: <u>0.00</u> TONS
TOTAL STEAM FLOW: <u>2824.0</u> KLB TOTAL REFUSE PR. <u>443.6</u> TONS	GROSS REFUSE REC: <u>716.08</u> TONS NON PROCESSED: <u>0.00</u> TONS ✓ FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>716.08</u> TONS ✓	WELL WATER USE: ENDING: <u>402343000</u> GAL BEGINNING: <u>402043000</u> GAL TOTAL USED: <u>300000</u> GAL	EOM OUT: <u>20.83</u>
EST PIT INVENTORY: <u>2,374.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>176.30</u>	MEDICAL WASTE: PROCESSED: <u>10.57</u> TONS % OF REFUSE PROC: <u>2.38</u> %	UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>91.3</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>530.8</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>649.3</u> TOT STM TO T/G: <u>2,820.0</u>
UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>91.4</u> % LB STEAM/GROSS KW <u>9.8</u> LB LIME/TON PR.: <u>5.7</u>			

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 02, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1449.0</u> KLB FEEDWATER USED: <u>1497.0</u> KLB	STEAM PRODUCED: <u>1517.0</u> KLB FEEDWATER USED: <u>1546.0</u> KLB	GENERATOR OUT: ENDING: <u>8006.0</u> WH TOT BEGINNING: <u>7996.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173800</u> CU FT ENDING: <u>173804</u> CU FT TOTAL USED: <u>4</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>48</u> KLB BLOWDOWN : <u>3.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>29</u> KLB BLOWDOWN : <u>1.9</u> %	UTILITY OUT: ENDING: <u>6177410</u> JEM TOT BEGINNING: <u>5923760</u> JEM TOT TOTAL: <u>253.7</u> MWH	PEBBLE LIME : ENDING: <u>7.2</u> FT/IN OUT BEGINNING: <u>6.5</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>73112.5</u> HRS BEGINNING: <u>73088.5</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>72082.2</u> HRS BEGINNING: <u>72058.2</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>7.17</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>60.4</u> KLB/HR APPROX REF PROC: <u>223.0</u> TONS REFUSE PROCESSED: <u>241.5</u> TONS	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>63.2</u> KLB/HR APPROX REF PROC: <u>224.0</u> TONS REFUSE PROCESSED: <u>252.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>34.4</u> MWH KWH/TON: <u>75.6</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2986.0</u> KLB TOTAL REFUSE PR. <u>454.5</u> TONS	GROSS REFUSE REC: <u>694.05</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>694.05</u> TONS ✓		CARBON INVENTORY: ENDING: <u>20</u> FT. OUT <u>0</u> IN OUT BEGINNING: <u>20</u> FT. OUT <u>10</u> IN OUT RECEIVED: <u>0.00</u> TONS
WELL WATER USE: ENDING: <u>402651000</u> GAL BEGINNING: <u>402343000</u> GAL TOTAL USED: <u>308000</u> GAL	EST PIT INVENTORY: <u>2,645.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>139.55</u>	MEDICAL WASTE : PROCESSED: <u>7.48</u> TONS % OF REFUSE PROC: <u>1.65</u> %	EOM OUT: <u>20.00</u>
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>93.8</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>558.1</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>98.1</u> % LB STEAM/GROSS KW <u>10.3</u> LB LIME/TON PR.: <u>4.8</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>633.7</u> TOT STM TO T/G: <u>2,965.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 03, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1450.0</u> KLB	STEAM PRODUCED: <u>1541.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1497.0</u> KLB	FEEDWATER USED: <u>1570.0</u> KLB	ENDING: <u>8017.0</u> WH TOT	BEGINNING: <u>173804</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8008.0</u> WH TOT	ENDING: <u>173860</u> CU FT
BLOWDOWN: <u>47</u> KLB	BLOWDOWN: <u>29</u> KLB	TOTAL: <u>316.8</u> MWH	TOTAL USED: <u>56</u> CU FT
BLOWDOWN: <u>3.1</u> %	BLOWDOWN: <u>1.8</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>6433710</u> JEM TOT	ENDING: <u>4.1</u> FT/IN OUT
ENDING: <u>73136.5</u> HRS	ENDING: <u>72108.2</u> HRS	BEGINNING: <u>6177410</u> JEM TOT	BEGINNING: <u>7.2</u> FT/IN OUT
BEGINNING: <u>73112.5</u> HRS	BEGINNING: <u>72082.2</u> HRS	TOTAL: <u>256.3</u> MWH	RECEIVED: <u>24.78</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>4.08</u>
AVG. STEAM FLOW: <u>60.4</u> KLB/HR	AVG. STEAM FLOW: <u>64.2</u> KLB/HR	ENDING: <u>2801500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>224.0</u> TONS	APPROX REF PROC: <u>227.0</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>289</u> LBS
REFUSE PROCESSED: <u>241.7</u> TONS	REFUSE PROCESSED: <u>256.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>289</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2991.0</u> KLB	GROSS REFUSE REC: <u>610.74</u> TONS	IN PLANT USE: <u>60.5</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>458.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>132.1</u>	ENDING: <u>19</u> FT. OUT <u>90</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>19.98</u> TONS ✓		BEGINNING: <u>20</u> FT. OUT <u>0</u> IN OUT
ENDING: <u>402860000</u> GAL	TOTAL REFUSE REC: <u>590.78</u> TONS ✓	MEDICAL WASTE:	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>402651000</u> GAL	EST PIT INVENTORY: <u>2,781.0</u> TONS	PROCESSED: <u>6.99</u> TONS	EOM OUT: <u>26.50</u>
TOTAL USED: <u>309000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.53</u> %	
	<u>127.04</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>93.8</u> %	UNIT 2 % MCR: <u>99.7</u> %	TG % MCR: <u>84.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>8.4</u>	GROSS KW/TON PR. <u>691.7</u>	
NET KWH/TON PR. <u>559.6</u>	LB LIME/TON PR.: <u>86.9</u>	TOT STM TO T/G: <u>2,998.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 04, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1423.0</u> KLB	STEAM PRODUCED: <u>1538.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1472.0</u> KLB	FEEDWATER USED: <u>1567.0</u> KLB	ENDING: <u>8027.0</u> WH TOT	BEGINNING: <u>173860</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8017.0</u> WH TOT	ENDING: <u>173861</u> CU FT
BLOWDOWN: <u>49</u> KLB	BLOWDOWN: <u>31</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>2.0</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>6684660</u> JEM TOT	ENDING: <u>4.7</u> FT/IN OUT
ENDING: <u>73160.5</u> HRS	ENDING: <u>72130.0</u> HRS	BEGINNING: <u>6433710</u> JEM TOT	BEGINNING: <u>4.1</u> FT/IN OUT
BEGINNING: <u>73136.5</u> HRS	BEGINNING: <u>72108.2</u> HRS	TOTAL: <u>251.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.8</u> HRS	UTILITY IN:	EOM OUT: <u>4.58</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.3</u> KLB/HR	AVG. STEAM FLOW: <u>64.0</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>219.5</u> TONS	APPROX REF PROC: <u>233.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>237.2</u> TONS	REFUSE PROCESSED: <u>258.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>536</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>37.1</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2959.0</u> KLB	GROSS REFUSE REC: <u>607.93</u> TONS	KWH/TON: <u>80.9</u>	ENDING: <u>19</u> FT. OUT <u>71</u> IN OUT
TOTAL REFUSE PR. <u>457.9</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>19</u> FT. OUT <u>80</u> IN OUT
	FERROUS HAULED: <u>22.77</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>585.16</u> TONS ✓		EOM OUT: <u>24.92</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,742.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>403255000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>4.62</u> TONS	
BEGINNING: <u>402860000</u> GAL	<u>103.67</u>	% OF REFUSE PROC: <u>1.01</u> %	
TOTAL USED: <u>295000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>92.1</u> %	UNIT 2 % MCR: <u>99.4</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.3</u>	GROSS KW/TON PR. <u>828.9</u>	
NET KWH/TON PR. <u>548.0</u>	LB LIME/TON PR.: <u>4.1</u>	TOT STM TO T/G: <u>2,950.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 05, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1433.0</u> KLB	STEAM PRODUCED: <u>1514.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1481.0</u> KLB	FEEDWATER USED: <u>1543.0</u> KLB	ENDING: <u>8037.0</u> WH TOT	BEGINNING: <u>173861</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8027.0</u> WH TOT	ENDING: <u>173861</u> CU FT
BLOWDOWN: <u>48</u> KLB	BLOWDOWN: <u>29</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN %: <u>3.2</u> %	BLOWDOWN %: <u>1.9</u> %	UTILITY OUT:	
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>6932200</u> JEM TOT	PEBBLE LIME:
ENDING: <u>73184.5</u> HRS	ENDING: <u>72154.0</u> HRS	BEGINNING: <u>6684660</u> JEM TOT	ENDING: <u>4.9</u> FT/IN OUT
BEGINNING: <u>73160.5</u> HRS	BEGINNING: <u>72130.0</u> HRS	TOTAL: <u>247.5</u> MWH	BEGINNING: <u>4.7</u> FT/IN OUT
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		RECEIVED: <u>0.00</u> TONS
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>4.75</u>
AVG. STEAM FLOW: <u>59.7</u> KLB/HR	AVG. STEAM FLOW: <u>63.1</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	
APPROX REF PROC: <u>211.6</u> TONS	APPROX REF PROC: <u>218.1</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	CARBON USAGE:
REFUSE PROCESSED: <u>238.8</u> TONS	REFUSE PROCESSED: <u>252.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #1: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	USAGE UNIT #2: <u>269</u> LBS
TOTAL STEAM FLOW: <u>2947.0</u> KLB	GROSS REFUSE REC: <u>580.56</u> TONS	IN PLANT USE: <u>40.5</u> MWH	DAILY TOTAL: <u>538</u> LBS
TOTAL REFUSE PR. <u>440.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS ✓	KWH/TON: <u>92.0</u>	CARBON INVENTORY:
<i>501.37</i>	FERROUS HAULED: <u>0.00</u> TONS ✓		ENDING: <u>19</u> FT. OUT <u>71</u> IN OUT
WELL WATER USE:	TOTAL REFUSE REC: <u>580.56</u> TONS		BEGINNING: <u>19</u> FT. OUT <u>71</u> IN OUT
ENDING: <u>403541000</u> GAL	EST PIT INVENTORY: <u>3,034.0</u> TONS	MEDICAL WASTE:	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>403255000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>10.29</u> TONS	EOM OUT: <u>24.92</u>
TOTAL USED: <u>286000</u> GAL	<i>126.77</i>	% OF REFUSE PROC: <u>2.34</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>92.7</u> %	UNIT 2 % MCR: <u>98.0</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>654.6</u>	
NET KWH/TON PR. <u>582.6</u>	LB LIME/TON PR.: <u>1.4</u>	TOT STM TO T/G: <u>2,934.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 08, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1411.0</u> KLB FEEDWATER USED: <u>1459.0</u> KLB	STEAM PRODUCED: <u>1516.0</u> KLB FEEDWATER USED: <u>1546.0</u> KLB	GENERATOR OUT: ENDING: <u>8047.0</u> WH TOT BEGINNING: <u>8037.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173861</u> CU FT ENDING: <u>173862</u> CU FT TOTAL USED: <u>1</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>48</u> KLB BLOWDOWN: <u>3.3</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>30</u> KLB BLOWDOWN: <u>1.9</u> %	UTILITY OUT: ENDING: <u>7179000</u> JEM TOT BEGINNING: <u>6932200</u> JEM TOT TOTAL: <u>246.8</u> MWH	PEBBLE LIME : ENDING: <u>5.0</u> FT/IN OUT BEGINNING: <u>4.9</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>73208.5</u> HRS BEGINNING: <u>73184.5</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>72177.9</u> HRS BEGINNING: <u>72154.0</u> HRS TOTAL: <u>23.9</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>5.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>58.8</u> KLB/HR	AVG. STEAM FLOW: <u>63.2</u> KLB/HR	IN PLANT USE: <u>41.2</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>222.0</u> TONS	APPROX REF PROC: <u>207.0</u> TONS	KWH/TON: <u>96.0</u>	CARBON INVENTORY: ENDING: <u>19</u> FT. OUT <u>66</u> IN OUT BEGINNING: <u>19</u> FT. OUT <u>71</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>235.2</u> TONS	REFUSE PROCESSED: <u>252.7</u> TONS		EOM OUT: <u>24.50</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2927.0</u> KLB TOTAL REFUSE PR. <u>429.0</u> TONS <u>487.9</u>	GROSS REFUSE REC: <u>224.98</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>224.98</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	
WELL WATER USE: ENDING: <u>403816000</u> GAL BEGINNING: <u>403541000</u> GAL TOTAL USED: <u>275000</u> GAL	EST PIT INVENTORY: <u>2,450.0</u> TONS ASH HAULED: <u>0.00</u> TONS ✓		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>91.3</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>575.3</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>98.1</u> % LB STEAM/GROSS KW <u>10.2</u> LB LIME/TON PR.: <u>0.7</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>671.3</u> TOT STM TO T/G: <u>2,916.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 07, 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1415.0</u> KLB FEEDWATER USED: <u>1462.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>47</u> KLB BLOWDOWN : <u>3.2</u> %</p> <p>GRATE RUN TIME: ENDING: <u>73232.5</u> HRS BEGINNING: <u>73208.5</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>59.0</u> KLB/HR APPROX REF PROC: <u>230.0</u> TONS REFUSE PROCESSED: <u>235.8</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2949.0</u> KLB TOTAL REFUSE PR. <u>451.0</u> TONS <i>491.5</i></p> <p>WELL WATER USE: ENDING: <u>404099000</u> GAL BEGINNING: <u>403816000</u> GAL TOTAL USED: <u>283000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>91.6</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>550.4</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1534.0</u> KLB FEEDWATER USED: <u>1564.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>30</u> KLB BLOWDOWN : <u>1.9</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72201.9</u> HRS BEGINNING: <u>72177.9</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>63.9</u> KLB/HR APPROX REF PROC: <u>221.0</u> TONS REFUSE PROCESSED: <u>255.7</u> TONS</p> <p>GROSS REFUSE REC: <u>0.00</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>0.00</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>1,867.0</u> TONS ✓ ASH HAULED: <u>0.00</u> TONS ✓</p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>99.2</u> % LB STEAM/GROSS KW <u>9.3</u> LB LIME/TON PR.: <u>2.1</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>8058.0</u> WH TOT BEGINNING: <u>8047.0</u> WH TOT TOTAL: <u>316.8</u> MWH</p> <p>UTILITY OUT: ENDING: <u>7427250</u> JEM TOT BEGINNING: <u>7179000</u> JEM TOT TOTAL: <u>248.3</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>68.8</u> MWH KWH/TON: <u>152.0</u></p> <p>MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>84.1</u> % GROSS KW/TON PR. <u>702.4</u> TOT STM TO T/G: <u>2,942.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173862</u> CU FT ENDING: <u>173864</u> CU FT TOTAL USED: <u>2</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>5.3</u> FT/IN OUT BEGINNING: <u>5.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>5.25</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>19</u> FT. OUT <u>39</u> IN OUT BEGINNING: <u>19</u> FT. OUT <u>66</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>22.25</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 08 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1420.5</u> KLB	STEAM PRODUCED: <u>1487.7</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1469.4</u> KLB	FEEDWATER USED: <u>1518.4</u> KLB	ENDING: <u>8067.0</u> WH TOT	BEGINNING: <u>173864</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8058.0</u> WH TOT	ENDING: <u>173864</u> CU FT
BLOWDOWN: <u>49</u> KLB	BLOWDOWN: <u>31</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>2.0</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>7668140</u> JEM TOT	ENDING: <u>6.0</u> FT/IN OUT
ENDING: <u>73256.5</u> HRS	ENDING: <u>72225.9</u> HRS	BEGINNING: <u>7427250</u> JEM TOT	BEGINNING: <u>5.3</u> FT/IN OUT
BEGINNING: <u>73232.5</u> HRS	BEGINNING: <u>72201.9</u> HRS	TOTAL: <u>240.9</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>6.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.2</u> KLB/HR	AVG. STEAM FLOW: <u>62.0</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>216.2</u> TONS	APPROX REF PROC: <u>219.1</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>236.8</u> TONS	REFUSE PROCESSED: <u>248.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>18.3</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>41.1</u>	ENDING: <u>19</u> FT. OUT <u>39</u> IN OUT
TOTAL STEAM FLOW: <u>2908.2</u> KLB	GROSS REFUSE REC: <u>736.91</u> TONS		BEGINNING: <u>19</u> FT. OUT <u>66</u> IN OUT
TOTAL REFUSE PR. <u>445.2</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS		EOM OUT: <u>22.25</u>
ENDING: <u>404399000</u> GAL	TOTAL REFUSE REC: <u>736.91</u> TONS ✓	MEDICAL WASTE:	
BEGINNING: <u>404099000</u> GAL	EST PIT INVENTORY: <u>2,314.0</u> TONS	PROCESSED: <u>9.94</u> TONS	
TOTAL USED: <u>300000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.23</u> %	
	<u>168.58</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>91.9</u> %	UNIT 2 % MCR: <u>96.3</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>11.2</u>	GROSS KW/TON PR. <u>582.2</u>	
NET KWH/TON PR. <u>541.0</u>	LB LIME/TON PR.: <u>4.9</u>	TOT STM TO T/G: <u>2,879.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 09 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1393.5</u> KLB	STEAM PRODUCED: <u>1535.6</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1441.2</u> KLB	FEEDWATER USED: <u>1565.5</u> KLB	ENDING: <u>8078.0</u> WH TOT	BEGINNING: <u>173864</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8067.0</u> WH TOT	ENDING: <u>173890</u> CU FT
BLOWDOWN: <u>48</u> KLB	BLOWDOWN: <u>30</u> KLB	TOTAL: <u>316.8</u> MWH	TOTAL USED: <u>26</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>1.9</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>7911980</u> JEM TOT	ENDING: <u>6.1</u> FT/IN OUT
ENDING: <u>73280.5</u> HRS	ENDING: <u>72249.9</u> HRS	BEGINNING: <u>7688140</u> JEM TOT	BEGINNING: <u>8.0</u> FT/IN OUT
BEGINNING: <u>73256.5</u> HRS	BEGINNING: <u>72225.9</u> HRS	TOTAL: <u>243.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>6.08</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>58.1</u> KLB/HR	AVG. STEAM FLOW: <u>64.0</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>221.7</u> TONS	APPROX REF PROC: <u>228.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>232.3</u> TONS	REFUSE PROCESSED: <u>255.9</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>73.0</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2929.1</u> KLB	GROSS REFUSE REC: <u>654.59</u> TONS	KWH/TON: <u>157.4</u>	ENDING: <u>19</u> FT. OUT <u>39</u> IN OUT
TOTAL REFUSE PR. <u>463.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>19</u> FT. OUT <u>39</u> IN OUT
<u>501.88</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	TOTAL REFUSE REC: <u>654.59</u> TONS ✓	MEDICAL WASTE:	EOM OUT: <u>22.25</u>
ENDING: <u>404712000</u> GAL	EST PIT INVENTORY: <u>2,879.0</u> TONS	PROCESSED: <u>13.68</u> TONS	
BEGINNING: <u>404399000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.95</u> %	
TOTAL USED: <u>313000</u> GAL	<u>112.43</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>90.2</u> %	UNIT 2 % MCR: <u>99.4</u> %	TG % MCR: <u>84.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.2</u>	GROSS KW/TON PR. <u>683.3</u>	
NET KWH/TON PR. <u>525.9</u>	LB LIME/TON PR.: <u>0.7</u>	TOT STM TO T/G: <u>2,904.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE: MARCH 10 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1395.6</u> KLB	STEAM PRODUCED: <u>1550.8</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1442.2</u> KLB	FEEDWATER USED: <u>1582.2</u> KLB	ENDING: <u>8088.0</u> WH TOT	BEGINNING: <u>173890</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8078.0</u> WH TOT	ENDING: <u>173891</u> CU FT
BLOWDOWN: <u>47</u> KLB	BLOWDOWN: <u>31</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN %: <u>3.2</u> %	BLOWDOWN %: <u>2.0</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>8160900</u> JEM TOT	ENDING: <u>4.3</u> FT/IN OUT
ENDING: <u>73304.5</u> HRS	ENDING: <u>72273.9</u> HRS	BEGINNING: <u>7911980</u> JEM TOT	BEGINNING: <u>6.1</u> FT/IN OUT
BEGINNING: <u>73280.5</u> HRS	BEGINNING: <u>72249.9</u> HRS	TOTAL: <u>248.9</u> MWH	RECEIVED: <u>19.49</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>4.25</u>
AVG. STEAM FLOW: <u>58.2</u> KLB/HR	AVG. STEAM FLOW: <u>64.6</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>223.0</u> TONS	APPROX REF PROC: <u>228.0</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>232.6</u> TONS	REFUSE PROCESSED: <u>258.5</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
		IN PLANT USE: <u>39.1</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>85.2</u>	ENDING: <u>18</u> FT. OUT <u>95</u> IN OUT
TOTAL STEAM FLOW: <u>2946.4</u> KLB	GROSS REFUSE REC: <u>575.51</u> TONS		BEGINNING: <u>19</u> FT. OUT <u>39</u> IN OUT
TOTAL REFUSE PR. <u>458.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>25.92</u>
	TOTAL REFUSE REC: <u>575.51</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>2,900.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>405031000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>7.44</u> TONS	
BEGINNING: <u>404712000</u> GAL		% OF REFUSE PROC: <u>1.62</u> %	
TOTAL USED: <u>319000</u> GAL	<u>178.86</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>90.3</u> %	UNIT 2 % MCR: <u>100.3</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>628.2</u>	
NET KWH/TON PR. <u>542.9</u>	LB LIME/TON PR.: <u>72.7</u>	TOT STM TO T/G: <u>2,934.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE: MARCH 11 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1348.3</u> KLB	STEAM PRODUCED: <u>1521.7</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1393.8</u> KLB	FEEDWATER USED: <u>1550.7</u> KLB	ENDING: <u>8098.0</u> WH TOT	BEGINNING: <u>173890</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8088.0</u> WH TOT	ENDING: <u>173890</u> CU FT
BLOWDOWN: <u>46</u> KLB	BLOWDOWN: <u>29</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN %: <u>3.3</u> %	BLOWDOWN %: <u>1.9</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>8402300</u> JEM TOT	ENDING: <u>6.3</u> FT/IN OUT
ENDING: <u>73328.5</u> HRS	ENDING: <u>72297.9</u> HRS	BEGINNING: <u>8160900</u> JEM TOT	BEGINNING: <u>4.3</u> FT/IN OUT
BEGINNING: <u>73304.5</u> HRS	BEGINNING: <u>72273.9</u> HRS	TOTAL: <u>241.4</u> MWH	RECEIVED: <u>19.49</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>6.25</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>56.2</u> KLB/HR	AVG. STEAM FLOW: <u>63.4</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>224.0</u> TONS	APPROX REF PROC: <u>240.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>224.7</u> TONS	REFUSE PROCESSED: <u>253.6</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>46.6</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2870.0</u> KLB	GROSS REFUSE REC: <u>588.22</u> TONS	GEN. WHTON: <u>99.4</u>	ENDING: <u>19</u> FT. OUT <u>14</u> IN OUT
TOTAL REFUSE PR. <u>468.6</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>19</u> FT. OUT <u>39</u> IN OUT
<u>482.9</u>	FERROUS HAULED: <u>19.11</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>569.11</u> TONS <u>564.11</u>		EOM OUT: <u>20.31</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,801.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>405340000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>4.62</u> TONS	
BEGINNING: <u>405031000</u> GAL		% OF REFUSE PROC: <u>0.99</u> %	
TOTAL USED: <u>309000</u> GAL	<u>189.42</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>87.2</u> %	UNIT 2 % MCR: <u>98.5</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.0</u>	GROSS KW/TON PR. <u>614.8</u>	
NET KW/TON PR. <u>515.1</u>	LB LIME/TON PR.: <u>98.6</u>	TOT STM TO T/G: <u>2,833.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 12 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1392.2</u> KLB FEEDWATER USED: <u>1440.3</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>48</u> KLB BLOWDOWN: <u>3.3</u> %</p> <p>GRATE RUN TIME: ENDING: <u>73352.5</u> HRS BEGINNING: <u>73328.5</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>58.0</u> KLB/HR APPROX REF PROC: <u>183.0</u> TONS REFUSE PROCESSED: <u>232.0</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2924.8</u> KLB TOTAL REFUSE PR. <u>394.6</u> TONS 497.96</p> <p>WELL WATER USE: ENDING: <u>405649000</u> GAL BEGINNING: <u>405340000</u> GAL TOTAL USED: <u>309000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>90.1</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>626.5</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1532.6</u> KLB FEEDWATER USED: <u>1564.1</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>32</u> KLB BLOWDOWN: <u>2.0</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72321.9</u> HRS BEGINNING: <u>72297.9</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>63.9</u> KLB/HR APPROX REF PROC: <u>201.0</u> TONS REFUSE PROCESSED: <u>255.4</u> TONS</p> <p>GROSS REFUSE REC: <u>599.78</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>17.24</u> TONS ✓ TOTAL REFUSE REC: <u>582.54</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>2,976.0</u> TONS ASH HAULED: <u>0.00</u> TONS ✓</p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>99.2</u> % LB STEAM/GROSS KW <u>10.2</u> LB LIME/TON PR.: <u>100.4</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>8108.0</u> WH TOT BEGINNING: <u>8098.0</u> WH TOT TOTAL: <u>288.0</u> MWH</p> <p>UTILITY OUT: ENDING: <u>8649500</u> JEM TOT BEGINNING: <u>8402300</u> JEM TOT TOTAL: <u>247.2</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>40.8</u> MWH KWH/TON: <u>103.4</u></p> <p>MEDICAL WASTE : PROCESSED: <u>10.56</u> TONS % OF REFUSE PROC: <u>2.68</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>728.9</u> TOT 8TM TO T/G: <u>2,886.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173890</u> CU FT ENDING: <u>173893</u> CU FT TOTAL USED: <u>3</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>6.5</u> FT/IN OUT BEGINNING: <u>6.3</u> FT/IN OUT RECEIVED: <u>19.49</u> TONS</p> <p>EOM OUT: <u>6.42</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS</p> <p>DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>18</u> FT. OUT <u>55</u> IN OUT BEGINNING: <u>19</u> FT. OUT <u>14</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>22.58</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 13 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1392.6</u> KLB FEEDWATER USED: <u>1439.7</u> KLB	STEAM PRODUCED: <u>1535.4</u> KLB FEEDWATER USED: <u>1580.8</u> KLB	GENERATOR OUT: ENDING: <u>8118.0</u> WH TOT BEGINNING: <u>8108.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173893</u> CU FT ENDING: <u>173912</u> CU FT TOTAL USED: <u>19</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>47</u> KLB BLOWDOWN: <u>3.3</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>45</u> KLB BLOWDOWN: <u>2.9</u> %	UTILITY OUT: ENDING: <u>8899370</u> JEM TOT BEGINNING: <u>8849500</u> JEM TOT TOTAL: <u>249.9</u> MWH	PEBBLE LIME: ENDING: <u>6.6</u> FT/IN OUT BEGINNING: <u>6.5</u> FT/IN OUT RECEIVED: <u>19.49</u> TONS
GRATE RUN TIME: ENDING: <u>73378.5</u> HRS BEGINNING: <u>73352.5</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>72345.9</u> HRS BEGINNING: <u>72321.9</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>6.50</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>58.0</u> KLB/HR	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>64.0</u> KLB/HR	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>38.1</u> MWH KWH/TON: <u>91.4</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>199.3</u> TONS REFUSE PROCESSED: <u>232.1</u> TONS	APPROX REF PROC: <u>202.9</u> TONS REFUSE PROCESSED: <u>255.9</u> TONS		CARBON INVENTORY: ENDING: <u>18</u> FT. OUT <u>32</u> IN OUT BEGINNING: <u>18</u> FT. OUT <u>55</u> IN OUT RECEIVED: <u>0.00</u> TONS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			EOM OUT: <u>20.67</u>
TOTAL STEAM FLOW: <u>2928.0</u> KLB TOTAL REFUSE PR. <u>417.3</u> TONS 503.19	GROSS REFUSE REC: <u>304.32</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>304.32</u> TONS ✓	MEDICAL WASTE: PROCESSED: <u>15.19</u> TONS % OF REFUSE PROC: <u>3.64</u> %	
WELL WATER USE: ENDING: <u>405960000</u> GAL BEGINNING: <u>405649000</u> GAL TOTAL USED: <u>311000</u> GAL	EST PIT INVENTORY: <u>2,771.0</u> TONS ASH HAULED: <u>0.00</u> TONS 106.09		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>90.1</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>598.7</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>99.3</u> % LB STEAM/GROSS KW <u>10.2</u> LB LIME/TON PR.: <u>84.2</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>690.1</u> TOT STM TO T/G: <u>2,928.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#2 SIM Totalizer OUT OF SERVICE

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 14 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1368.2</u> KLB FEEDWATER USED: <u>1417.1</u> KLB	STEAM PRODUCED: <u>1544.0</u> KLB FEEDWATER USED: <u>1574.5</u> KLB	GENERATOR OUT: ENDING: <u>8128.0</u> WH TOT BEGINNING: <u>8118.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173912</u> CU FT ENDING: <u>173917</u> CU FT TOTAL USED: <u>5</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>49</u> KLB BLOWDOWN: <u>3.5</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>31</u> KLB BLOWDOWN: <u>1.9</u> %	UTILITY OUT: ENDING: <u>9137560</u> JEM TOT BEGINNING: <u>8689370</u> JEM TOT TOTAL: <u>238.2</u> MWH	PEBBLE LIME : ENDING: <u>7.5</u> FT/IN OUT BEGINNING: <u>6.6</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>73400.5</u> HRS BEGINNING: <u>73376.5</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>72369.9</u> HRS BEGINNING: <u>72345.9</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>7.42</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>57.0</u> KLB/HR	AVG. STEAM FLOW: <u>64.3</u> KLB/HR	IN PLANT USE: <u>49.8</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>225.4</u> TONS	APPROX REF PROC: <u>218.5</u> TONS	KWH/TON: <u>112.2</u>	CARBON INVENTORY: ENDING: <u>18</u> FT. OUT <u>26</u> IN OUT BEGINNING: <u>18</u> FT. OUT <u>32</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>228.0</u> TONS	REFUSE PROCESSED: <u>257.3</u> TONS		EOM OUT: <u>20.17</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2912.2</u> KLB TOTAL REFUSE PR. <u>444.0</u> TONS	GROSS REFUSE REC: <u>0.00</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>0.00</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	
WELL WATER USE: ENDING: <u>406288000</u> GAL BEGINNING: <u>405986000</u> GAL TOTAL USED: <u>309000</u> GAL	EST PIT INVENTORY: <u>2,176.0</u> TONS ASH HAULED: <u>0.00</u> TONS ✓		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>88.5</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>536.5</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>99.9</u> % LB STEAM/GROSS KW <u>10.1</u> LB LIME/TON PR.: <u>6.4</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>648.7</u> TOT STM TO T/G: <u>2,847.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#2 STM Flow Totalizer O/S

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 15 1999

BOILER NO. 1
STEAM PRODUCED: 1352.5 KLB
FEEDWATER USED: 1397.9 KLB

BOILER BLOWDOWN:
BLOWDOWN: 45 KLB
BLOWDOWN: 3.2 %

GRATE RUN TIME:
ENDING: 73424.5 HRS
BEGINNING: 73400.5 HRS
TOTAL: 24.0 HRS

BOILER RUN TIME: 24.0 HRS

AVG. STEAM FLOW: 56.4 KLB/HR

APPROX REF PROC: 231.2 TONS

REFUSE PROCESSED: 225.4 TONS

NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB

TOTAL STEAM FLOW: 2757.4 KLB
TOTAL REFUSE PR. 457.3 TONS

477.68

WELL WATER USE:
ENDING: 408561000 GAL
BEGINNING: 406269000 GAL
TOTAL USED: 2292000 GAL

UNIT 1 AVAILABILITY: 100.0 %
UNIT 1 % MCR: 87.5 %
LB STEAM/LB PR. 3.0
NET KWH/TON PR. 520.9

BOILER NO. 2
STEAM PRODUCED: 1404.9 KLB
FEEDWATER USED: 1444.9 KLB

BOILER BLOWDOWN:
BLOWDOWN: 40 KLB
BLOWDOWN: 2.8 %

GRATE RUN TIME:
ENDING: 72393.9 HRS
BEGINNING: 72369.9 HRS
TOTAL: 24.0 HRS

BOILER RUN TIME: 24.0 HRS

AVG. STEAM FLOW: 58.5 KLB/HR

APPROX REF PROC: 213.8 TONS

REFUSE PROCESSED: 234.2 TONS

GROSS REFUSE REC: 729.95 TONS
NON PROCESSED: 0.00 TONS
FERROUS HAULED: 0.00 TONS
TOTAL REFUSE REC: 729.95 TONS

729.89

EST PIT INVENTORY: 2,828.0 TONS
ASH HAULED: 0.00 TONS

174.20

UNIT 2 AVAILABILITY: 100.0 %
UNIT 2 % MCR: 90.9 %
LB STEAM/GROSS KW 9.6
LB LIME/TON PR.: -4.8

ELECTRICITY
GENERATOR OUT:
ENDING: 8138.0 WH TOT
BEGINNING: 8128.0 WH TOT
TOTAL: 288.0 MWH

UTILITY OUT:
ENDING: 9137560 JEM TOT
BEGINNING: 8899370 JEM TOT
TOTAL: 238.2 MWH

UTILITY IN:
ENDING: 2601500 JEM TOT
BEGINNING: 2601500 JEM TOT
TOTAL: 0.0 MWH

GENERATOR RUN TIME: 24.0 HRS
IN PLANT USE: 49.8 MWH
KWH/TON: 108.9

MEDICAL WASTE :
PROCESSED: 12.28 TONS
% OF REFUSE PROC: 2.69 %

TG AVAILABILITY: 100.0 %
TG % MCR: 76.4 %
GROSS KW/TON PR. 629.8
TOT STM TO T/G: 2,741.0

INVENTORY
NATURAL GAS USAGE:
BEGINNING: 173917 CU FT
ENDING: 173918 CU FT
TOTAL USED: 1 CU FT

PEBBLE LIME :
ENDING: 5.1 FT/IN OUT
BEGINNING: 5.8 FT/IN OUT
RECEIVED: 0.00 TONS

EOM OUT: 5.08

CARBON USAGE:
USAGE UNIT #1: 269 LBS
USAGE UNIT #2: 269 LBS

DAILY TOTAL: 538 LBS

CARBON INVENTORY:
ENDING: 18 FT. OUT 7 IN OUT
BEGINNING: 18 FT. OUT 28 IN OUT
RECEIVED: 0.00 TONS

EOM OUT: 18.58

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 16 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1332.4</u> KLB FEEDWATER USED: <u>1381.3</u> KLB	STEAM PRODUCED: <u>1450.0</u> KLB FEEDWATER USED: <u>1485.0</u> KLB	GENERATOR OUT: ENDING: <u>8148.0</u> WH TOT BEGINNING: <u>8138.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173918</u> CU FT ENDING: <u>173918</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>49</u> KLB BLOWDOWN: <u>3.5</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>35</u> KLB BLOWDOWN: <u>2.4</u> %	UTILITY OUT: ENDING: <u>9599070</u> JEM TOT BEGINNING: <u>9386020</u> JEM TOT TOTAL: <u>233.1</u> MWH	PEBBLE LIME : ENDING: <u>6.0</u> FT/IN OUT BEGINNING: <u>5.1</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>73448.5</u> HRS BEGINNING: <u>73424.5</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>72417.9</u> HRS BEGINNING: <u>72393.9</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>6.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>55.0</u> MWH KWH/TON: <u>117.2</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>55.5</u> KLB/HR	AVG. STEAM FLOW: <u>60.4</u> KLB/HR		DAILY TOTAL: <u>536</u> LBS
APPROX REF PROC: <u>223.8</u> TONS	APPROX REF PROC: <u>247.4</u> TONS		CARBON INVENTORY: ENDING: <u>18</u> FT. OUT <u>2</u> IN OUT BEGINNING: <u>18</u> FT. OUT <u>7</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>222.1</u> TONS	REFUSE PROCESSED: <u>241.7</u> TONS		EOM OUT: <u>18.17</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2782.4</u> KLB TOTAL REFUSE PR. <u>468.8</u> TONS	GROSS REFUSE REC: <u>686.86</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS TOTAL REFUSE REC: <u>686.86</u> TONS ✓		
WELL WATER USE: ENDING: <u>406882000</u> GAL BEGINNING: <u>406561000</u> GAL TOTAL USED: <u>301000</u> GAL	EST PIT INVENTORY: <u>2,723.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>127.23</u>	MEDICAL WASTE : PROCESSED: <u>5.07</u> TONS % OF REFUSE PROC: <u>1.08</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>86.2</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>497.1</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>93.8</u> % LB STEAM/GROSS KW <u>9.7</u> LB LIME/TON PR.: <u>6.0</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>614.3</u> TOT STM TO T/G: <u>2,782.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

*STM & F.W. Flows out of service to J. Ginger for Calibration
Estimated F.W. use & STM produced
as.*

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 17 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1333.5</u> KLB FEEDWATER USED: <u>1381.9</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>48</u> KLB BLOWDOWN: <u>3.5</u> %</p> <p>GRATE RUN TIME: ENDING: <u>73472.5</u> HRS BEGINNING: <u>73448.5</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>55.6</u> KLB/HR APPROX REF PROC: <u>205.0</u> TONS REFUSE PROCESSED: <u>222.3</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2871.9</u> KLB TOTAL REFUSE PR. <u>451.8</u> TONS 986.98</p> <p>WELL WATER USE: ENDING: <u>407168000</u> GAL BEGINNING: <u>406862000</u> GAL TOTAL USED: <u>306000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>86.3</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>522.0</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1538.4</u> KLB FEEDWATER USED: <u>1583.9</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>28</u> KLB BLOWDOWN: <u>1.8</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72441.9</u> HRS BEGINNING: <u>72417.9</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>64.1</u> KLB/HR APPROX REF PROC: <u>238.6</u> TONS REFUSE PROCESSED: <u>258.4</u> TONS</p> <p>GROSS REFUSE REC: <u>608.37</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>18.28</u> TONS ✓ TOTAL REFUSE REC: <u>590.09</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>3,132.0</u> TONS ASH HAULED: <u>0.00</u> TONS 107.39</p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>99.5</u> % LB STEAM/GROSS KW <u>10.0</u> LB LIME/TON PR.: <u>71.8</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>8158.0</u> WH TOT BEGINNING: <u>8148.0</u> WH TOT TOTAL: <u>288.0</u> MWH</p> <p>UTILITY OUT: ENDING: <u>9834930</u> JEM TOT BEGINNING: <u>9599070</u> JEM TOT TOTAL: <u>235.9</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>52.1</u> MWH KWH/TON: <u>115.4</u></p> <p>MEDICAL WASTE : PROCESSED: <u>8.28</u> TONS % OF REFUSE PROC: <u>1.83</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>78.4</u> % GROSS KW/TON PR. <u>637.4</u> TOT STM TO T/G: <u>2,821.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173918</u> CU FT ENDING: <u>173918</u> CU FT TOTAL USED: <u>0</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>2.0</u> FT/IN OUT BEGINNING: <u>6.0</u> FT/IN OUT RECEIVED: <u>22.46</u> TONS</p> <p>EOM OUT: <u>2.00</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>18</u> FT. OUT <u>31</u> IN OUT BEGINNING: <u>18</u> FT. OUT <u>2</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>20.58</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

24 hours #2 steam flow totalizer out of service.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE March 18, 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1332.0</u> KLB FEEDWATER USED: <u>1378.8</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>47</u> KLB BLOWDOWN: <u>3.4</u> %</p> <p>GRATE RUN TIME: ENDING: <u>73496.5</u> HRS BEGINNING: <u>73472.5</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>55.5</u> KLB/HR</p> <p>APPROX REF PROC: <u>210.0</u> TONS</p> <p>REFUSE PROCESSED: <u>222.0</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2860.8</u> KLB TOTAL REFUSE PR. <u>423.2</u> TONS</p> <p>WELL WATER USE: ENDING: <u>407476000</u> GAL BEGINNING: <u>407168000</u> GAL TOTAL USED: <u>308000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>86.2</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>559.2</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1528.8</u> KLB FEEDWATER USED: <u>1543.2</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>14</u> KLB BLOWDOWN: <u>0.9</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72465.7</u> HRS BEGINNING: <u>72441.9</u> HRS TOTAL: <u>23.8</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>63.7</u> KLB/HR</p> <p>APPROX REF PROC: <u>208.0</u> TONS</p> <p>REFUSE PROCESSED: <u>254.8</u> TONS</p> <p>GROSS REFUSE REC: <u>589.42</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>19.14</u> TONS ✓ TOTAL REFUSE REC: <u>550.28</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>2,742.0</u> TONS ASH HAULED: <u>0.00</u> TONS</p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>88.9</u> % LB STEAM/GROSS KW <u>11.0</u> LB LIME/TON PR.: <u>12.4</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>8167.0</u> WH TOT BEGINNING: <u>8158.0</u> WH TOT TOTAL: <u>259.2</u> MWH</p> <p>UTILITY OUT: ENDING: <u>10071550</u> JEM TOT BEGINNING: <u>9834930</u> JEM TOT TOTAL: <u>236.8</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>22.8</u> MWH KWH/TON: <u>53.4</u></p> <p>MEDICAL WASTE: PROCESSED: <u>1.17</u> TONS % OF REFUSE PROC: <u>1.89</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>612.5</u> TOT STM TO T/G: <u>2,810.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173918</u> CU FT ENDING: <u>173951</u> CU FT TOTAL USED: <u>33</u> CU FT</p> <p>PEBBLE LIME: ENDING: <u>3.7</u> FT/IN OUT BEGINNING: <u>2.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>3.56</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>289</u> LBS USAGE UNIT #2: <u>289</u> LBS DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>17</u> FT. OUT <u>75</u> IN OUT BEGINNING: <u>18</u> FT. OUT <u>31</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>23.25</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

24 hours #2 steam flow totalizer out of service.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE March 19, 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1325.2</u> KLB FEEDWATER USED: <u>1374.9</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>50</u> KLB BLOWDOWN: <u>3.6</u> %</p> <p>GRATE RUN TIME: ENDING: <u>73520.5</u> HRS BEGINNING: <u>73496.5</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>55.2</u> KLB/HR APPROX REF PROC: <u>210.0</u> TONS REFUSE PROCESSED: <u>220.9</u> TONS</p> <p>TOTAL STEAM FLOW: <u>2815.6</u> KLB TOTAL REFUSE PR. <u>432.4</u> TONS <u>472.9</u></p> <p>WELL WATER USE: ENDING: <u>407763000</u> GAL BEGINNING: <u>407476000</u> GAL TOTAL USED: <u>287000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>85.7</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>531.9</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1490.4</u> KLB FEEDWATER USED: <u>1504.3</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>14</u> KLB BLOWDOWN: <u>0.9</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72489.7</u> HRS BEGINNING: <u>72465.7</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>62.1</u> KLB/HR APPROX REF PROC: <u>207.0</u> TONS REFUSE PROCESSED: <u>248.4</u> TONS</p> <p>GROSS REFUSE REC: <u>637.27</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>637.27</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>3,034.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>174.92</u></p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>96.4</u> % LB STEAM/GROSS KW <u>9.8</u> LB LIME/TON PR.: <u>6.5</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>8177.0</u> WH TOT BEGINNING: <u>8167.0</u> WH TOT TOTAL: <u>288.0</u> MWH</p> <p>UTILITY OUT: ENDING: <u>301570</u> JEM TOT BEGINNING: <u>71550</u> JEM TOT TOTAL: <u>230.0</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>58.0</u> MWH KWH/TON: <u>134.1</u></p> <p>MEDICAL WASTE : PROCESSED: <u>15.42</u> TONS % OF REFUSE PROC: <u>3.57</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>666.0</u> TOT STM TO T/G: <u>2,745.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>173951</u> CU FT ENDING: <u>173951</u> CU FT TOTAL USED: <u>0</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>4.6</u> FT/IN OUT BEGINNING: <u>3.7</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>4.50</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS</p> <p>DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>17</u> FT. OUT <u>75</u> IN OUT BEGINNING: <u>17</u> FT. OUT <u>75</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>23.25</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

24 hours #2 steam flow totalizer out of service.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE March 20, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1345.4</u> KLB FEEDWATER USED: <u>1393.0</u> KLB	STEAM PRODUCED: <u>1472.1</u> KLB FEEDWATER USED: <u>1514.2</u> KLB	GENERATOR OUT: ENDING: <u>8186.0</u> WH TOT BEGINNING: <u>8177.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173951</u> CU FT ENDING: <u>173951</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>48</u> KLB BLOWDOWN: <u>3.4</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>42</u> KLB BLOWDOWN: <u>2.8</u> %	UTILITY OUT: ENDING: <u>535310</u> JEM TOT BEGINNING: <u>301570</u> JEM TOT TOTAL: <u>233.7</u> MWH	PEBBLE LIME : ENDING: <u>4.7</u> FT/IN OUT BEGINNING: <u>4.6</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>73544.5</u> HRS BEGINNING: <u>73520.5</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>72513.7</u> HRS BEGINNING: <u>72489.7</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>4.58</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>58.1</u> KLB/HR APPROX REF PROC: <u>228.0</u> TONS	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>61.3</u> KLB/HR APPROX REF PROC: <u>212.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>25.5</u> MWH KWH/TON: <u>57.2</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
REFUSE PROCESSED: <u>* 224.2</u> TONS NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB	REFUSE PROCESSED: <u>* 245.3</u> TONS GROSS REFUSE REC: <u>268.48</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>268.48</u> TONS ✓		CARBON INVENTORY: ENDING: <u>17</u> FT. OUT <u>18</u> IN OUT BEGINNING: <u>17</u> FT. OUT <u>75</u> IN OUT RECEIVED: <u>0.00</u> TONS
TOTAL STEAM FLOW: <u>2817.5</u> KLB TOTAL REFUSE PR. <u>445.1</u> TONS <u>471.6</u>	EST PIT INVENTORY: <u>2,800.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>129.77</u>	MEDICAL WASTE : PROCESSED: <u>* 5.08</u> TONS % OF REFUSE PROC: <u>1.14</u> %	EOM OUT: <u>18.50</u>
WELL WATER USE: ENDING: <u>408078000</u> GAL BEGINNING: <u>407763000</u> GAL TOTAL USED: <u>315000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>87.0</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>525.2</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>95.2</u> % LB STEAM/GROSS KW <u>10.9</u> LB LIME/TON PR.: <u>0.7</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>582.4</u> TOT STM TO T/G: <u>2,785.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE March 21, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1348.8</u> KLB FEEDWATER USED: <u>1394.7</u> KLB	STEAM PRODUCED: <u>1444.7</u> KLB FEEDWATER USED: <u>1521.9</u> KLB	GENERATOR OUT: ENDING: <u>8198.0</u> WH TOT BEGINNING: <u>8186.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173951</u> CU FT ENDING: <u>173951</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>48</u> KLB BLOWDOWN: <u>3.4</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>77</u> KLB BLOWDOWN: <u>5.1</u> %	UTILITY OUT: ENDING: <u>771910</u> JEM TOT BEGINNING: <u>535310</u> JEM TOT TOTAL: <u>236.8</u> MWH	PEBBLE LIME : ENDING: <u>4.8</u> FT/IN OUT BEGINNING: <u>4.7</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>73568.5</u> HRS BEGINNING: <u>73544.5</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>72537.8</u> HRS BEGINNING: <u>72513.7</u> HRS TOTAL: <u>23.9</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>4.87</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>51.4</u> MWH KWH/TON: <u>110.5</u>	CARBON USAGE: USAGE UNIT #1: <u>289</u> LBS USAGE UNIT #2: <u>289</u> LBS
AVG. STEAM FLOW: <u>56.1</u> KLB/HR	AVG. STEAM FLOW: <u>60.2</u> KLB/HR		DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>225.0</u> TONS	APPROX REF PROC: <u>242.0</u> TONS		CARBON INVENTORY: ENDING: <u>18</u> FT. OUT <u>89</u> IN OUT BEGINNING: <u>17</u> FT. OUT <u>18</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>224.5</u> TONS	REFUSE PROCESSED: <u>240.8</u> TONS		EOM OUT: <u>23.42</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2791.5</u> KLB TOTAL REFUSE PR. <u>465.3</u> TONS	GROSS REFUSE REC: <u>0.00</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>0.00</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	
WELL WATER USE: ENDING: <u>408378000</u> GAL BEGINNING: <u>408078000</u> GAL TOTAL USED: <u>301000</u> GAL	EST PIT INVENTORY: <u>2,509.0</u> TONS ASH HAULED: <u>0.00</u> TONS ✓		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>87.1</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>508.5</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>93.5</u> % LB STEAM/GROSS KW <u>9.7</u> LB LIME/TON PR.: <u>0.7</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>619.0</u> TOT STM TO T/G: <u>2,803.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 22, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1319.5</u> KLB	STEAM PRODUCED: <u>1492.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1365.5</u> KLB	FEEDWATER USED: <u>1564.7</u> KLB	ENDING: <u>8206.0</u> WH TOT	BEGINNING: <u>173951</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8196.0</u> WH TOT	ENDING: <u>173951</u> CU FT
BLOWDOWN: <u>46</u> KLB	BLOWDOWN: <u>73</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.4</u> %	BLOWDOWN: <u>4.6</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1009120</u> JEM TOT	ENDING: <u>5.2</u> FT/IN OUT
ENDING: <u>73592.5</u> HRS	ENDING: <u>72561.5</u> HRS	BEGINNING: <u>771910</u> JEM TOT	BEGINNING: <u>4.8</u> FT/IN OUT
BEGINNING: <u>73588.5</u> HRS	BEGINNING: <u>72537.6</u> HRS	TOTAL: <u>237.2</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.9</u> HRS	UTILITY IN:	EOM OUT: <u>5.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.0</u> KLB/HR	AVG. STEAM FLOW: <u>62.2</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>289</u> LBS
APPROX REF PROC: <u>214.0</u> TONS	APPROX REF PROC: <u>226.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>*219.9</u> TONS	REFUSE PROCESSED: <u>*248.7</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>50.8</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2811.5</u> KLB	GROSS REFUSE REC: <u>824.60</u> TONS	KWH/TON: <u>112.3</u>	ENDING: <u>16</u> FT. OUT <u>85</u> IN OUT
TOTAL REFUSE PR. <u>452.4</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>16</u> FT. OUT <u>89</u> IN OUT
<u>482.96</u>	FERROUS HAULED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	TOTAL REFUSE REC: <u>824.60</u> TONS <u>815.40</u>	MEDICAL WASTE:	EOM OUT: <u>23.08</u>
ENDING: <u>408687000</u> GAL	EST PIT INVENTORY: <u>3,015.0</u> TONS	PROCESSED: <u>*12.38</u> TONS	
BEGINNING: <u>408379000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.73</u> %	
TOTAL USED: <u>308000</u> GAL	<u>176.09</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.4</u> %	UNIT 2 % MCR: <u>98.5</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>0.8</u>	GROSS KW/TON PR. <u>636.7</u>	
NET KWH/TON PR. <u>524.4</u>	LB LIME/TON PR.: <u>2.8</u>	TOT STM TO T/G: <u>2,820.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 23, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1321.2</u> KLB	STEAM PRODUCED: <u>1494.4</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1367.8</u> KLB	FEEDWATER USED: <u>1567.7</u> KLB	ENDING: <u>8216.0</u> WH TOT	BEGINNING: <u>173951</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8206.0</u> WH TOT	ENDING: <u>173952</u> CU FT
BLOWDOWN: <u>47</u> KLB	BLOWDOWN: <u>73</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>3.4</u> %	BLOWDOWN: <u>4.7</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1245390</u> JEM TOT	ENDING: <u>5.7</u> FT/IN OUT
ENDING: <u>73618.5</u> HRS	ENDING: <u>72585.5</u> HRS	BEGINNING: <u>1009120</u> JEM TOT	BEGINNING: <u>5.2</u> FT/IN OUT
BEGINNING: <u>73592.5</u> HRS	BEGINNING: <u>72581.5</u> HRS	TOTAL: <u>236.3</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>5.58</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.1</u> KLB/HR	AVG. STEAM FLOW: <u>62.3</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>222.4</u> TONS	APPROX REF PROC: <u>234.7</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>220.2</u> TONS	REFUSE PROCESSED: <u>249.1</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>51.7</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>110.0</u>	ENDING: <u>16</u> FT. OUT <u>83</u> IN OUT
TOTAL STEAM FLOW: <u>2815.6</u> KLB	GROSS REFUSE REC: <u>650.41</u> TONS		BEGINNING: <u>16</u> FT. OUT <u>85</u> IN OUT
TOTAL REFUSE PR. <u>470.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>22.92</u>
	TOTAL REFUSE REC: <u>650.41</u> TONS ✓	MEDICAL WASTE:	
WELL WATER USE:	EST PIT INVENTORY: <u>3,229.0</u> TONS	PROCESSED: <u>13.39</u> TONS	
ENDING: <u>408991000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.85</u> %	
BEGINNING: <u>408687000</u> GAL	<u>128.77</u>		
TOTAL USED: <u>304000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.5</u> %	UNIT 2 % MCR: <u>98.7</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.8</u>	GROSS KW/TON PR. <u>612.2</u>	
NET KWH/TON PR. <u>502.2</u>	LB LIME/TON PR.: <u>3.3</u>	TOT STM TO T/G: <u>2,818.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 24, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1317.9</u> KLB FEEDWATER USED: <u>1365.3</u> KLB	STEAM PRODUCED: <u>1501.9</u> KLB FEEDWATER USED: <u>1573.2</u> KLB	GENERATOR OUT: ENDING: <u>8226.0</u> WH TOT BEGINNING: <u>6216.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173952</u> CU FT ENDING: <u>173960</u> CU FT TOTAL USED: <u>8</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>47</u> KLB BLOWDOWN: <u>3.5</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>71</u> KLB BLOWDOWN: <u>4.5</u> %	UTILITY OUT: ENDING: <u>1486210</u> JEM TOT BEGINNING: <u>1245390</u> JEM TOT TOTAL: <u>240.8</u> MWH	PEBBLE LIME: ENDING: <u>2.7</u> FT/IN OUT BEGINNING: <u>5.7</u> FT/IN OUT RECEIVED: <u>24.62</u> TONS
GRATE RUN TIME: ENDING: <u>73640.4</u> HRS BEGINNING: <u>73616.5</u> HRS TOTAL: <u>23.9</u> HRS	GRATE RUN TIME: ENDING: <u>72609.5</u> HRS BEGINNING: <u>72585.5</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>2.58</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>54.9</u> KLB/HR	AVG. STEAM FLOW: <u>62.6</u> KLB/HR	IN PLANT USE: <u>47.2</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>217.8</u> TONS	APPROX REF PROC: <u>228.0</u> TONS	KWH/TON: <u>104.1</u>	CARBON INVENTORY: ENDING: <u>16</u> FT. OUT <u>80</u> IN OUT BEGINNING: <u>16</u> FT. OUT <u>83</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>*219.7</u> TONS	REFUSE PROCESSED: <u>*250.3</u> TONS		EOM OUT: <u>22.67</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2819.8</u> KLB TOTAL REFUSE PR. <u>453.1</u> TONS <u>476.31</u>	GROSS REFUSE REC: <u>543.21</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>543.21</u> TONS ✓	MEDICAL WASTE: PROCESSED: <u>*8.31</u> TONS % OF REFUSE PROC: <u>1.39</u> %	
WELL WATER USE: ENDING: <u>408301000</u> GAL BEGINNING: <u>408891000</u> GAL TOTAL USED: <u>310000</u> GAL	EST PIT INVENTORY: <u>3,287.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>153.56</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>85.3</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>531.5</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>97.2</u> % LB STEAM/GROSS KW <u>9.8</u> LB LIME/TON PR.: <u>87.9</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>78.4</u> % GROSS KW/TON PR. <u>635.8</u> TOT STM TO T/G: <u>2,829.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

Received 3538.63 tons for the week
Processed 40.57 tons for the week

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE March 25, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1336.2</u> KLB	STEAM PRODUCED: <u>1493.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1384.3</u> KLB	FEEDWATER USED: <u>1562.2</u> KLB	ENDING: <u>8236.0</u> WH TOT	BEGINNING: <u>173960</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8226.0</u> WH TOT	ENDING: <u>173960</u> CU FT
BLOWDOWN: <u>48</u> KLB	BLOWDOWN: <u>69</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.5</u> %	BLOWDOWN: <u>4.4</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1730260</u> JEM TOT	ENDING: <u>3.2</u> FT/IN OUT
ENDING: <u>73664.4</u> HRS	ENDING: <u>72633.5</u> HRS	BEGINNING: <u>1486210</u> JEM TOT	BEGINNING: <u>2.7</u> FT/IN OUT
BEGINNING: <u>73640.4</u> HRS	BEGINNING: <u>72609.5</u> HRS	TOTAL: <u>244.1</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>3.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.7</u> KLB/HR	AVG. STEAM FLOW: <u>62.2</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>223.0</u> TONS	APPROX REF PROC: <u>218.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>222.7</u> TONS	REFUSE PROCESSED: <u>248.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>44.0</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>97.8</u>	ENDING: <u>16</u> FT. OUT <u>80</u> IN OUT
TOTAL STEAM FLOW: <u>2829.1</u> KLB	GROSS REFUSE REC: <u>641.16</u> TONS		BEGINNING: <u>16</u> FT. OUT <u>80</u> IN OUT
TOTAL REFUSE PR. <u>449.6</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>17.30</u> TONS ✓		EOM OUT: <u>22.67</u>
	TOTAL REFUSE REC: <u>623.86</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>3,384.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>409606000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>8.59</u> TONS	
BEGINNING: <u>409301000</u> GAL		% OF REFUSE PROC: <u>1.91</u> %	
TOTAL USED: <u>306000</u> GAL	<u>116.61</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>86.5</u> %	UNIT 2 % MCR: <u>96.6</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.8</u>	GROSS KW/TON PR. <u>640.8</u>	
NET KWH/TON PR. <u>542.8</u>	LB LIME/TON PR.: <u>3.5</u>	TOT STM TO T/G: <u>2,841.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE March 26, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1348.9</u> KLB FEEDWATER USED: <u>1397.3</u> KLB	STEAM PRODUCED: <u>1474.4</u> KLB FEEDWATER USED: <u>1501.6</u> KLB	GENERATOR OUT: ENDING: <u>8246.0</u> WH TOT BEGINNING: <u>8236.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173960</u> CU FT ENDING: <u>173960</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>48</u> KLB BLOWDOWN: <u>3.5</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>27</u> KLB BLOWDOWN: <u>1.8</u> %	UTILITY OUT: ENDING: <u>1972820</u> JEM TOT BEGINNING: <u>1730260</u> JEM TOT TOTAL: <u>242.6</u> MWH	PEBBLE LIME : ENDING: <u>3.7</u> FT/IN OUT BEGINNING: <u>3.2</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>73688.3</u> HRS BEGINNING: <u>73684.4</u> HRS TOTAL: <u>23.9</u> HRS	GRATE RUN TIME: ENDING: <u>72657.5</u> HRS BEGINNING: <u>72633.5</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2801500</u> JEM TOT BEGINNING: <u>2801500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>3.58</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>56.2</u> KLB/HR	AVG. STEAM FLOW: <u>61.4</u> KLB/HR	IN PLANT USE: <u>45.4</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>226.0</u> TONS	APPROX REF PROC: <u>225.0</u> TONS	KWH/TON: <u>98.5</u>	CARBON INVENTORY: ENDING: <u>16</u> FT. OUT <u>51</u> IN OUT BEGINNING: <u>16</u> FT. OUT <u>80</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>224.8</u> TONS	REFUSE PROCESSED: <u>245.7</u> TONS		EOM OUT: <u>20.25</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2823.3</u> KLB TOTAL REFUSE PR. <u>461.5</u> TONS	GROSS REFUSE REC: <u>609.56</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>609.56</u> TONS ✓		
WELL WATER USE: <u>482.2</u>	EST PIT INVENTORY: <u>3,559.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>100.0</u>	MEDICAL WASTE : PROCESSED: <u>10.50</u> TONS % OF REFUSE PROC: <u>2.28</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>87.3</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>525.8</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>95.4</u> % LB STEAM/GROSS KW <u>9.8</u> LB LIME/TON PR.: <u>3.4</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>624.1</u> TOT STM TO T/G: <u>2,840.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 27, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1328.4</u> KLB	STEAM PRODUCED: <u>1478.1</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1375.9</u> KLB	FEEDWATER USED: <u>1542.4</u> KLB	ENDING: <u>8256.0</u> WH TOT	BEGINNING: <u>173960</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8246.0</u> WH TOT	ENDING: <u>173963</u> CU FT
BLOWDOWN: <u>48</u> KLB	BLOWDOWN: <u>64</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>3</u> CU FT
BLOWDOWN: <u>3.5</u> %	BLOWDOWN: <u>4.2</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2210980</u> JEM TOT	ENDING: <u>3.9</u> FT/IN OUT
ENDING: <u>73712.3</u> HRS	ENDING: <u>72681.5</u> HRS	BEGINNING: <u>1972820</u> JEM TOT	BEGINNING: <u>3.7</u> FT/IN OUT
BEGINNING: <u>73688.3</u> HRS	BEGINNING: <u>72657.5</u> HRS	TOTAL: <u>238.2</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>3.75</u>
AVG. STEAM FLOW: <u>55.4</u> KLB/HR	AVG. STEAM FLOW: <u>61.6</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>221.8</u> TONS	APPROX REF PROC: <u>238.8</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>221.4</u> TONS	REFUSE PROCESSED: <u>248.4</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2806.5</u> KLB	GROSS REFUSE REC: <u>334.16</u> TONS	IN PLANT USE: <u>49.8</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>485.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>107.0</u>	ENDING: <u>16</u> FT. OUT <u>28</u> IN OUT
WELL WATER USE: <u>493.5</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>16</u> FT. OUT <u>51</u> IN OUT
ENDING: <u>410209000</u> GAL	TOTAL REFUSE REC: <u>334.16</u> TONS ✓	MEDICAL WASTE:	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>409914000</u> GAL	EST PIT INVENTORY: <u>3,404.0</u> TONS ✓	PROCESSED: <u>5.30</u> TONS	EOM OUT: <u>18.33</u>
TOTAL USED: <u>295000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	% OF REFUSE PROC: <u>1.14</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.9</u> %	UNIT 2 % MCR: <u>95.6</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.7</u>	GROSS KW/TON PR. <u>618.4</u>	
NET KWH/TON PR. <u>511.4</u>	LB LIME/TON PR.: <u>1.3</u>	TOT STM TO T/G: <u>2,801.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE MARCH 28, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1324.0</u> KLB	STEAM PRODUCED: <u>1478.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1372.0</u> KLB	FEEDWATER USED: <u>1532.0</u> KLB	ENDING: <u>8266.0</u> WH TOT	BEGINNING: <u>173963</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8256.0</u> WH TOT	ENDING: <u>173963</u> CU FT
BLOWDOWN: <u>48</u> KLB	BLOWDOWN: <u>58</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.5</u> %	BLOWDOWN: <u>3.7</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2448000</u> JEM TOT	ENDING: <u>4.6</u> FT/IN OUT
ENDING: <u>73738.3</u> HRS	ENDING: <u>72705.4</u> HRS	BEGINNING: <u>2210980</u> JEM TOT	BEGINNING: <u>3.9</u> FT/IN OUT
BEGINNING: <u>73712.3</u> HRS	BEGINNING: <u>72681.5</u> HRS	TOTAL: <u>237.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.9</u> HRS	UTILITY IN:	EOM OUT: <u>4.50</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.2</u> KLB/HR	AVG. STEAM FLOW: <u>61.5</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>221.9</u> TONS	APPROX REF PROC: <u>227.5</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>220.7</u> TONS	REFUSE PROCESSED: <u>246.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>51.0</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>113.5</u>	ENDING: <u>16</u> FT. OUT <u>5</u> IN OUT
TOTAL STEAM FLOW: <u>2800.0</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS		BEGINNING: <u>16</u> FT. OUT <u>28</u> IN OUT
TOTAL REFUSE PR. <u>449.3</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>18.42</u>
	TOTAL REFUSE REC: <u>0.00</u> TONS ✓		
WELL WATER USE: <u>4166.7</u>	EST PIT INVENTORY: <u>2,820.0</u> TONS ✓	MEDICAL WASTE:	
ENDING: <u>410517000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>410209000</u> GAL		% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>308000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.7</u> %	UNIT 2 % MCR: <u>95.5</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.7</u>	GROSS KW/TON PR. <u>640.9</u>	
NET KWH/TON PR. <u>527.5</u>	LB LIME/TON PR.: <u>4.9</u>	TOT STM TO T/G: <u>2,785.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 29, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1325.2</u> KLB FEEDWATER USED: <u>1375.4</u> KLB	STEAM PRODUCED: <u>1479.3</u> KLB FEEDWATER USED: <u>1550.3</u> KLB	GENERATOR OUT: ENDING: <u>8275.0</u> WH TOT BEGINNING: <u>8266.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173963</u> CU FT ENDING: <u>173963</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>50</u> KLB BLOWDOWN: <u>3.6</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>71</u> KLB BLOWDOWN: <u>4.6</u> %	UTILITY OUT: ENDING: <u>2886810</u> JEM TOT BEGINNING: <u>2448000</u> JEM TOT TOTAL: <u>238.8</u> MWH	PEBBLE LIME : ENDING: <u>5.2</u> FT/IN OUT BEGINNING: <u>4.8</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>73760.3</u> HRS BEGINNING: <u>73736.3</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>72729.4</u> HRS BEGINNING: <u>72705.4</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>5.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>55.2</u> KLB/HR	AVG. STEAM FLOW: <u>61.6</u> KLB/HR	IN PLANT USE: <u>20.4</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>202.8</u> TONS	APPROX REF PROC: <u>222.2</u> TONS	KWH/TON: <u>46.3</u>	CARBON INVENTORY: ENDING: <u>16</u> FT. OUT <u>0</u> IN OUT BEGINNING: <u>16</u> FT. OUT <u>5</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>220.9</u> TONS	REFUSE PROCESSED: <u>246.6</u> TONS		EOM OUT: <u>16.00</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2804.5</u> KLB TOTAL REFUSE PR. <u>440.1</u> TONS	GROSS REFUSE REC: <u>648.92</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS TOTAL REFUSE REC: <u>648.92</u> TONS		
WELL WATER USE: ENDING: <u>410819000</u> GAL BEGINNING: <u>410517000</u> GAL TOTAL USED: <u>302000</u> GAL	EST PIT INVENTORY: <u>3,073.0</u> TONS ASH HAULED: <u>0.00</u> TONS	MEDICAL WASTE : PROCESSED: <u>15.10</u> TONS % OF REFUSE PROC: <u>3.43</u> %	
	<u>149.12</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>85.7</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>542.7</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>95.7</u> % LB STEAM/GROSS KW <u>10.8</u> LB LIME/TON PR.: <u>4.3</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>589.0</u> TOT STM TO T/G: <u>2,821.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 30, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1323.8</u> KLB	STEAM PRODUCED: <u>1474.8</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1380.9</u> KLB	FEEDWATER USED: <u>1549.7</u> KLB	ENDING: <u>8285.0</u> WH TOT	BEGINNING: <u>173983</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8275.0</u> WH TOT	ENDING: <u>173984</u> CU FT
BLOWDOWN: <u>57</u> KLB	BLOWDOWN: <u>75</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>4.1</u> %	BLOWDOWN: <u>4.8</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2923080</u> JEM TOT	ENDING: <u>5.4</u> FT/IN OUT
ENDING: <u>73784.3</u> HRS	ENDING: <u>72753.4</u> HRS	BEGINNING: <u>2686810</u> JEM TOT	BEGINNING: <u>5.2</u> FT/IN OUT
BEGINNING: <u>73760.3</u> HRS	BEGINNING: <u>72729.4</u> HRS	TOTAL: <u>236.3</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>5.33</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.2</u> KLB/HR	AVG. STEAM FLOW: <u>81.5</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>289</u> LBS
APPROX REF PROC: <u>193.5</u> TONS	APPROX REF PROC: <u>211.9</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>220.8</u> TONS	REFUSE PROCESSED: <u>245.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>51.7</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2798.4</u> KLB	GROSS REFUSE REC: <u>742.21</u> TONS	KWH/TON: <u>124.4</u>	ENDING: <u>15</u> FT. OUT <u>98</u> IN OUT
TOTAL REFUSE PR. <u>415.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>16</u> FT. OUT <u>0</u> IN OUT
<u>476.69</u>	FERROUS HAULED: <u>20.79</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	TOTAL REFUSE REC: <u>721.42</u> TONS ✓	MEDICAL WASTE:	EOM OUT: <u>23.17</u>
ENDING: <u>411119000</u> GAL	EST PIT INVENTORY: <u>3,404.0</u> TONS	PROCESSED: <u>10.29</u> TONS	
BEGINNING: <u>410819000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.48</u> %	
TOTAL USED: <u>300000</u> GAL	<u>124.08</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.8</u> %	UNIT 2 % MCR: <u>95.4</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.7</u>	GROSS KW/TON PR. <u>692.8</u>	
NET KWH/TON PR. <u>568.4</u>	LB LIME/TON PR.: <u>1.5</u>	TOT STM TO T/G: <u>2,822.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MARCH 31, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1320.0</u> KLB	STEAM PRODUCED: <u>1449.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1361.0</u> KLB	FEEDWATER USED: <u>1510.0</u> KLB	ENDING: <u>8295.0</u> WH TOT	BEGINNING: <u>173964</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8285.0</u> WH TOT	ENDING: <u>173964</u> CU FT
BLOWDOWN: <u>41</u> KLB	BLOWDOWN: <u>61</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.0</u> %	BLOWDOWN: <u>4.0</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3152250</u> JEM TOT	ENDING: <u>1.0</u> FT/IN OUT
ENDING: <u>73808.3</u> HRS	ENDING: <u>72777.4</u> HRS	BEGINNING: <u>2923080</u> JEM TOT	BEGINNING: <u>5.4</u> FT/IN OUT
BEGINNING: <u>73784.3</u> HRS	BEGINNING: <u>72753.4</u> HRS	TOTAL: <u>229.2</u> MWH	RECEIVED: <u>24.81</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>1.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.0</u> KLB/HR	AVG. STEAM FLOW: <u>60.4</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>177.6</u> TONS	APPROX REF PROC: <u>197.6</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>220.0</u> TONS	REFUSE PROCESSED: <u>241.5</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>58.8</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>153.6</u>	ENDING: <u>15</u> FT. OUT <u>91</u> IN OUT
TOTAL STEAM FLOW: <u>2769.0</u> KLB	GROSS REFUSE REC: <u>536.00</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>98</u> IN OUT
TOTAL REFUSE PR. <u>383.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
<u>469.32</u>	FERROUS HAULED: <u>0.00</u> TONS		EOM OUT: <u>22.58</u>
WELL WATER USE:	TOTAL REFUSE REC: <u>536.00</u> TONS <i>524.46</i>	MEDICAL WASTE:	
ENDING: <u>411421000</u> GAL	EST PIT INVENTORY: <u>3,540.0</u> TONS	PROCESSED: <u>7.82</u> TONS	
BEGINNING: <u>411119000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	% OF REFUSE PROC: <u>2.04</u> %	
TOTAL USED: <u>302000</u> GAL	<u>150.03</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.4</u> %	UNIT 2 % MCR: <u>93.8</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.6</u>	GROSS KW/TON PR. <u>752.0</u>	
NET KWH/TON PR. <u>598.4</u>	LB LIME/TON PR.: <u>93.5</u>	TOT STM TO T/G: <u>2,760.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 1, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1352.0</u> KLB FEEDWATER USED: <u>1413.0</u> KLB	STEAM PRODUCED: <u>1464.0</u> KLB FEEDWATER USED: <u>1537.0</u> KLB	GENERATOR OUT: ENDING: <u>8305.0</u> WH TOT BEGINNING: <u>8295.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>173964</u> CU FT ENDING: <u>173971</u> CU FT TOTAL USED: <u>7</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>61</u> KLB BLOWDOWN: <u>4.3</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>73</u> KLB BLOWDOWN: <u>4.7</u> %	UTILITY OUT: ENDING: <u>3386430</u> JEM TOT BEGINNING: <u>3152250</u> JEM TOT TOTAL: <u>234.2</u> MWH	PEBBLE LIME : ENDING: <u>1.1</u> FT/IN OUT BEGINNING: <u>1.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>73832.3</u> HRS BEGINNING: <u>73808.3</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>72801.4</u> HRS BEGINNING: <u>72777.4</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>1.08</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>53.8</u> MWH KWH/TON: <u>126.1</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
AVG. STEAM FLOW: <u>56.3</u> KLB/HR	AVG. STEAM FLOW: <u>61.0</u> KLB/HR		CARBON INVENTORY: ENDING: <u>15</u> FT. OUT <u>15</u> IN OUT BEGINNING: <u>15</u> FT. OUT <u>91</u> IN OUT RECEIVED: <u>0.00</u> TONS
APPROX REF PROC: <u>206.3</u> TONS	APPROX REF PROC: <u>209.3</u> TONS		EOM OUT: <u>16.25</u>
REFUSE PROCESSED: <u>225.3</u> TONS	REFUSE PROCESSED: <u>244.0</u> TONS		
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2818.0</u> KLB TOTAL REFUSE PR. <u>426.8</u> TONS	GROSS REFUSE REC: <u>276.51</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS TOTAL REFUSE REC: <u>276.51</u> TONS ✓		
	EST PIT INVENTORY: <u>3,209.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>218.14</u>	MEDICAL WASTE : PROCESSED: <u>11.16</u> TONS % OF REFUSE PROC: <u>2.62</u> %	
WELL WATER USE: <u>480.46</u> ENDING: <u>411725000</u> GAL BEGINNING: <u>411421000</u> GAL TOTAL USED: <u>304000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>87.5</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>548.7</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>94.7</u> % LB STEAM/GROSS KW <u>9.8</u> LB LIME/TON PR.: <u>0.7</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>674.9</u> TOT STM TO T/G: <u>2,830.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

Received 3,127 tons for the week
Processed tons for the week

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 2, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1382.0</u> KLB	STEAM PRODUCED: <u>1457.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1442.0</u> KLB	FEEDWATER USED: <u>1532.0</u> KLB	ENDING: <u>8315.0</u> WH TOT	BEGINNING: <u>173971</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8305.0</u> WH TOT	ENDING: <u>173972</u> CU FT
BLOWDOWN: <u>60</u> KLB	BLOWDOWN: <u>75</u> KLB	TOTAL: <u>286.0</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>4.2</u> %	BLOWDOWN: <u>4.9</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3626140</u> JEM TOT	ENDING: <u>1.5</u> FT/IN OUT
ENDING: <u>73856.3</u> HRS	ENDING: <u>72825.4</u> HRS	BEGINNING: <u>3386430</u> JEM TOT	BEGINNING: <u>1.1</u> FT/IN OUT
BEGINNING: <u>73832.3</u> HRS	BEGINNING: <u>72801.4</u> HRS	TOTAL: <u>239.7</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>1.42</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>57.6</u> KLB/HR	AVG. STEAM FLOW: <u>60.7</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>207.0</u> TONS	APPROX REF PROC: <u>237.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>230.3</u> TONS	REFUSE PROCESSED: <u>242.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>48.3</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2839.0</u> KLB	GROSS REFUSE REC: <u>268.38</u> TONS	KWH/TON: <u>105.5</u>	ENDING: <u>15</u> FT. OUT <u>15</u> IN OUT
TOTAL REFUSE PR. <u>457.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>15</u> IN OUT
	FERROUS HAULED: <u>2.56</u> TONS <i>20.56</i>		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>265.82</u> TONS <i>247.82</i>		EOM OUT: <u>16.25</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,820.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>412028000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	PROCESSED: <u>13.24</u> TONS	
BEGINNING: <u>411725000</u> GAL		% OF REFUSE PROC: <u>2.89</u> %	
TOTAL USED: <u>303000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>89.4</u> %	UNIT 2 % MCR: <u>94.3</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.9</u>	GROSS KW/TON PR. <u>629.5</u>	
NET KWH/TON PR. <u>523.9</u>	LB LIME/TON PR.: <u>2.7</u>	TOT STM TO T/G: <u>2,879.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 3, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1017.0</u> KLB	STEAM PRODUCED: <u>1482.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1055.0</u> KLB	FEEDWATER USED: <u>1533.0</u> KLB	ENDING: <u>8323.0</u> WH TOT	BEGINNING: <u>173972</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8315.0</u> WH TOT	ENDING: <u>174028</u> CU FT
BLOWDOWN: <u>38</u> KLB	BLOWDOWN: <u>51</u> KLB	TOTAL: <u>230.4</u> MWH	TOTAL USED: <u>56</u> CU FT
BLOWDOWN: <u>3.6</u> %	BLOWDOWN: <u>3.3</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3801940</u> JEM TOT	ENDING: <u>1.7</u> FT/IN OUT
ENDING: <u>73880.3</u> HRS	ENDING: <u>72849.4</u> HRS	BEGINNING: <u>3626140</u> JEM TOT	BEGINNING: <u>1.5</u> FT/IN OUT
BEGINNING: <u>73856.3</u> HRS	BEGINNING: <u>72825.4</u> HRS	TOTAL: <u>175.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>1.58</u>
BOILER RUN TIME: <u>17.4</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>58.4</u> KLB/HR	AVG. STEAM FLOW: <u>61.8</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>195</u> LBS
APPROX REF PROC: <u>128.3</u> TONS	APPROX REF PROC: <u>190.2</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>169.5</u> TONS	REFUSE PROCESSED: <u>247.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>464</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>54.6</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>168.4</u>	ENDING: <u>15</u> FT. OUT <u>15</u> IN OUT
TOTAL STEAM FLOW: <u>2499.0</u> KLB	GROSS REFUSE REC: <u>60.49</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>15</u> IN OUT
TOTAL REFUSE PR. <u>324.2</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>18.63</u> TONS ✓		EOM OUT: <u>16.25</u>
	TOTAL REFUSE REC: <u>41.86</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>2,701.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>412314000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>5.63</u> TONS	
BEGINNING: <u>412028000</u> GAL		% OF REFUSE PROC: <u>1.74</u> %	
TOTAL USED: <u>288000</u> GAL	<u>182.32</u>		
UNIT 1 AVAILABILITY: <u>72.5</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>65.8</u> %	UNIT 2 % MCR: <u>95.9</u> %	TG % MCR: <u>61.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.8</u>	GROSS KW/TON PR. <u>710.8</u>	
NET KWH/TON PR. <u>542.3</u>	LB LIME/TON PR.: <u>1.9</u>	TOT STM TO T/G: <u>2,400.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler off line at 1725 for scheduled outage.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 4, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>0.0</u> KLB	STEAM PRODUCED: <u>1430.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>0.0</u> KLB	FEEDWATER USED: <u>1468.0</u> KLB	ENDING: <u>8327.0</u> WH TOT	BEGINNING: <u>174028</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8323.0</u> WH TOT	ENDING: <u>174028</u> CU FT
BLOWDOWN: <u>0</u> KLB	BLOWDOWN: <u>38</u> KLB	TOTAL: <u>115.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN : <u>ERR</u> %	BLOWDOWN : <u>2.6</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3908700</u> JEM TOT	BEGINNING: <u>1.8</u> FT/IN OUT
ENDING: <u>73903.3</u> HRS	ENDING: <u>72872.4</u> HRS	BEGINNING: <u>3801940</u> JEM TOT	BEGINNING: <u>1.7</u> FT/IN OUT
BEGINNING: <u>73880.3</u> HRS	BEGINNING: <u>72849.4</u> HRS	TOTAL: <u>106.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>23.0</u> HRS	TOTAL: <u>23.0</u> HRS		
BOILER RUN TIME: <u>0.0</u> HRS	BOILER RUN TIME: <u>23.0</u> HRS	UTILITY IN:	EOM OUT: <u>1.67</u>
AVG. STEAM FLOW: <u>ERR</u> KLB/HR	AVG. STEAM FLOW: <u>62.2</u> KLB/HR	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>0.0</u> TONS	APPROX REF PROC: <u>156.2</u> TONS	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>0</u> LBS
REFUSE PROCESSED: <u>0.0</u> TONS	REFUSE PROCESSED: <u>238.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>258</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>23.0</u> HRS	DAILY TOTAL: <u>258</u> LBS
TOTAL STEAM FLOW: <u>1430.0</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS	IN PLANT USE: <u>8.4</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>156.2</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>54.0</u>	ENDING: <u>15</u> FT. OUT <u>15</u> IN OUT
<u>238.3</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>15</u> FT. OUT <u>15</u> IN OUT
WELL WATER USE:	TOTAL REFUSE REC: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
ENDING: <u>412520000</u> GAL	EST PIT INVENTORY: <u>2,334.0</u> TONS ✓	MEDICAL WASTE :	EOM OUT: <u>16.25</u>
BEGINNING: <u>412314000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	PROCESSED: <u>0.00</u> TONS	
TOTAL USED: <u>208000</u> GAL		% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>0.0</u> %	UNIT 2 AVAILABILITY: <u>95.8</u> %	TG AVAILABILITY: <u>95.8</u> %	
UNIT 1 % MCR: <u>0.0</u> %	UNIT 2 % MCR: <u>92.5</u> %	TG % MCR: <u>30.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>12.4</u>	GROSS KW/TON PR. <u>737.5</u>	
NET KWH/TON PR. <u>683.5</u>	LB LIME/TON PR.: <u>2.0</u>	TOT STM TO T/G: <u>1,182.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler off line for scheduled outage. #2 boiler 23 hours due to daylight savings time.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 05-99

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>0.0</u> KLB	STEAM PRODUCED: <u>1475.5</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>0.0</u> KLB	FEEDWATER USED: <u>1512.2</u> KLB	ENDING: <u>8332.0</u> WH TOT	BEGINNING: <u>174028</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8327.0</u> WH TOT	ENDING: <u>174028</u> CU FT
BLOWDOWN: <u>0</u> KLB	BLOWDOWN: <u>37</u> KLB	TOTAL: <u>144.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>ERR</u> %	BLOWDOWN: <u>2.4</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3998800</u> JEM TOT	ENDING: <u>1.8</u> FT/IN OUT
ENDING: <u>73903.3</u> HRS	ENDING: <u>72896.4</u> HRS	BEGINNING: <u>3908700</u> JEM TOT	BEGINNING: <u>1.8</u> FT/IN OUT
BEGINNING: <u>73880.3</u> HRS	BEGINNING: <u>72872.4</u> HRS	TOTAL: <u>90.1</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>23.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>1.67</u>
BOILER RUN TIME: <u>0.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>ERR</u> KLB/HR	AVG. STEAM FLOW: <u>61.5</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>0</u> LBS
APPROX REF PROC: <u>0.0</u> TONS	APPROX REF PROC: <u>227.5</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>0.0</u> TONS	REFUSE PROCESSED: <u>245.9</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>53.9</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>236.9</u>	ENDING: <u>15</u> FT. OUT <u>16</u> IN OUT
TOTAL STEAM FLOW: <u>1475.5</u> KLB	GROSS REFUSE REC: <u>364.35</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>15</u> IN OUT
TOTAL REFUSE PR. <u>227.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>16.33</u>
	TOTAL REFUSE REC: <u>364.35</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>2,567.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>412734000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>412520000</u> GAL		% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>214000</u> GAL	<u>128.39</u>		
UNIT 1 AVAILABILITY: <u>0.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>0.0</u> %	UNIT 2 % MCR: <u>95.5</u> %	TG % MCR: <u>38.2</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>632.9</u>	
NET KWH/TON PR. <u>396.0</u>	LB LIME/TON PR.: <u>0.0</u>	TOT STM TO T/G: <u>1,219.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler off line for scheduled outage. #2 boiler 23 hours due to daylight savings time.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 06 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>0.0</u> KLB FEEDWATER USED: <u>0.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>0</u> KLB BLOWDOWN : <u>ERR</u> %</p> <p>GRATE RUN TIME: ENDING: <u>73903.3</u> HRS BEGINNING: <u>73880.3</u> HRS TOTAL: <u>23.0</u> HRS</p> <p>BOILER RUN TIME: <u>0.0</u> HRS AVG. STEAM FLOW: <u>ERR</u> KLB/HR APPROX REF PROC: <u>0.0</u> TONS REFUSE PROCESSED: <u>0.0</u> TONS</p> <p>TOTAL STEAM FLOW: <u>1466.9</u> KLB TOTAL REFUSE PR. <u>211.8</u> TONS</p> <p>WELL WATER USE: ENDING: <u>412946000</u> GAL BEGINNING: <u>412734000</u> GAL TOTAL USED: <u>212000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>0.0</u> % UNIT 1 % MCR: <u>0.0</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>417.8</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1466.9</u> KLB FEEDWATER USED: <u>1501.7</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>35</u> KLB BLOWDOWN : <u>2.3</u> %</p> <p>GRATE RUN TIME: ENDING: <u>72920.4</u> HRS BEGINNING: <u>72896.4</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>61.1</u> KLB/HR APPROX REF PROC: <u>211.8</u> TONS REFUSE PROCESSED: <u>244.5</u> TONS</p> <p>GROSS REFUSE REC: <u>370.69</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>8.62</u> TONS ✓ TOTAL REFUSE REC: <u>362.07</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>2,859.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>12110</u></p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>94.9</u> % LB STEAM/GROSS KW <u>12.7</u> LB LIME/TON PR.: <u>11.9</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>8336.0</u> WH TOT BEGINNING: <u>8332.0</u> WH TOT TOTAL: <u>115.2</u> MWH</p> <p>UTILITY OUT: ENDING: <u>4087260</u> JEM TOT BEGINNING: <u>3998800</u> JEM TOT TOTAL: <u>88.5</u> MWH</p> <p>UTILITY IN: ENDING: <u>2601500</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>26.7</u> MWH KWH/TON: <u>126.2</u></p> <p>MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>30.6</u> % GROSS KW/TON PR. <u>543.9</u> TOT STM TO T/G: <u>1,210.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>174028</u> CU FT ENDING: <u>174029</u> CU FT TOTAL USED: <u>1</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>2.6</u> FT/IN OUT BEGINNING: <u>1.8</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>2.50</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>0</u> LBS USAGE UNIT #2: <u>269</u> LBS</p> <p>DAILY TOTAL: <u>269</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>15</u> FT. OUT <u>22</u> IN OUT BEGINNING: <u>15</u> FT. OUT <u>18</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>18.83</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler off line for scheduled outage

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 07 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>0.0</u> KLB	STEAM PRODUCED: <u>1439.3</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>0.0</u> KLB	FEEDWATER USED: <u>1473.9</u> KLB	ENDING: <u>8340.0</u> WH TOT	BEGINNING: <u>174029</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8336.0</u> WH TOT	ENDING: <u>174033</u> CU FT
BLOWDOWN: <u>0</u> KLB	BLOWDOWN: <u>35</u> KLB	TOTAL: <u>115.2</u> MWH	TOTAL USED: <u>4</u> CU FT
BLOWDOWN: <u>ERR</u> %	BLOWDOWN: <u>2.3</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4182060</u> JEM TOT	ENDING: <u>3.0</u> FT/IN OUT
ENDING: <u>73975.5</u> HRS	ENDING: <u>72944.4</u> HRS	BEGINNING: <u>4087260</u> JEM TOT	BEGINNING: <u>2.6</u> FT/IN OUT
BEGINNING: <u>73975.5</u> HRS	BEGINNING: <u>72920.4</u> HRS	TOTAL: <u>94.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>0.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>3.00</u>
BOILER RUN TIME: <u>0.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>ERR</u> KLB/HR	AVG. STEAM FLOW: <u>60.0</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>0</u> LBS
APPROX REF PROC: <u>0.0</u> TONS	APPROX REF PROC: <u>231.9</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>0.0</u> TONS	REFUSE PROCESSED: <u>239.9</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>20.4</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>88.0</u>	ENDING: <u>15</u> FT. OUT <u>22</u> IN OUT
TOTAL STEAM FLOW: <u>1439.3</u> KLB	GROSS REFUSE REC: <u>200.32</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>22</u> IN OUT
TOTAL REFUSE PR. <u>231.9</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>14.35</u> TONS ✓		EOM OUT: <u>16.83</u>
	TOTAL REFUSE REC: <u>185.97</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>2,490.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>413153000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>412946000</u> GAL		% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>207000</u> GAL			
UNIT 1 AVAILABILITY: <u>0.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>0.0</u> %	UNIT 2 % MCR: <u>93.1</u> %	TG % MCR: <u>30.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>12.5</u>	GROSS KW/TON PR. <u>496.8</u>	
NET KWH/TON PR. <u>408.8</u>	LB LIME/TON PR.: <u>5.4</u>	TOT STM TO T/G: <u>1,260.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler off line for scheduled outage

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 08, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>0.0</u> KLB	STEAM PRODUCED: <u>1391.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>0.0</u> KLB	FEEDWATER USED: <u>1433.0</u> KLB	ENDING: <u>8345.0</u> WH TOT	BEGINNING: <u>174033</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8340.0</u> WH TOT	ENDING: <u>174033</u> CU FT
BLOWDOWN: <u>0</u> KLB	BLOWDOWN: <u>42</u> KLB	TOTAL: <u>144.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN : <u>ERR</u> %	BLOWDOWN : <u>2.9</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4272800</u> JEM TOT	ENDING: <u>3.3</u> FT/IN OUT
ENDING: <u>73975.5</u> HRS	ENDING: <u>72968.4</u> HRS	BEGINNING: <u>4182060</u> JEM TOT	BEGINNING: <u>3.0</u> FT/IN OUT
BEGINNING: <u>73975.5</u> HRS	BEGINNING: <u>72944.4</u> HRS	TOTAL: <u>90.7</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>0.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>3.25</u>
BOILER RUN TIME: <u>0.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2601500</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>ERR</u> KLB/HR	AVG. STEAM FLOW: <u>58.0</u> KLB/HR	BEGINNING: <u>2601500</u> JEM TOT	USAGE UNIT #1: <u>0</u> LBS
APPROX REF PROC: <u>0.0</u> TONS	APPROX REF PROC: <u>212.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>0.0</u> TONS	REFUSE PROCESSED: <u>231.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>53.3</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>251.2</u>	ENDING: <u>15</u> FT. OUT <u>21</u> IN OUT
TOTAL STEAM FLOW: <u>1391.0</u> KLB	GROSS REFUSE REC: <u>309.65</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>22</u> IN OUT
TOTAL REFUSE PR. <u>212.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>16.75</u>
	TOTAL REFUSE REC: <u>309.65</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>2,742.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>413364000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>413153000</u> GAL		% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>211000</u> GAL	<u>140.93</u>		
UNIT 1 AVAILABILITY: <u>0.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>0.0</u> %	UNIT 2 % MCR: <u>90.0</u> %	TG % MCR: <u>38.2</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.7</u>	GROSS KW/TON PR. <u>679.2</u>	
NET KWH/TON PR. <u>428.0</u>	LB LIME/TON PR.: <u>4.4</u>	TOT STM TO T/G: <u>1,287.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler off line for scheduled outage

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 09 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>0.0</u> KLB FEEDWATER USED: <u>0.0</u> KLB	STEAM PRODUCED: <u>906.0</u> KLB FEEDWATER USED: <u>925.0</u> KLB	GENERATOR OUT: ENDING: <u>8347.0</u> WH TOT BEGINNING: <u>8345.0</u> WH TOT TOTAL: <u>57.6</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>174033</u> CU FT ENDING: <u>174064</u> CU FT TOTAL USED: <u>31</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>0</u> KLB BLOWDOWN : <u>ERR</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>19</u> KLB BLOWDOWN : <u>2.1</u> %	UTILITY OUT: ENDING: <u>4323080</u> JEM TOT BEGINNING: <u>4272800</u> JEM TOT TOTAL: <u>50.3</u> MWH	PEBBLE LIME : ENDING: <u>3.5</u> FT/IN OUT BEGINNING: <u>3.3</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>73975.5</u> HRS BEGINNING: <u>73975.5</u> HRS TOTAL: <u>0.0</u> HRS	GRATE RUN TIME: ENDING: <u>72992.4</u> HRS BEGINNING: <u>72968.4</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2611610</u> JEM TOT BEGINNING: <u>2601500</u> JEM TOT TOTAL: <u>10.1</u> MWH	EOM OUT: <u>3.42</u>
BOILER RUN TIME: <u>0.0</u> HRS AVG. STEAM FLOW: <u>ERR</u> KLB/HR APPROX REF PROC: <u>0.0</u> TONS REFUSE PROCESSED: <u>0.0</u> TONS	BOILER RUN TIME: <u>15.0</u> HRS AVG. STEAM FLOW: <u>60.3</u> KLB/HR APPROX REF PROC: <u>119.0</u> TONS REFUSE PROCESSED: <u>151.0</u> TONS	GENERATOR RUN TIME: <u>14.7</u> HRS IN PLANT USE: <u>17.4</u> MWH KWH/TON: <u>146.5</u>	CARBON USAGE: USAGE UNIT #1: <u>0</u> LBS USAGE UNIT #2: <u>168</u> LBS DAILY TOTAL: <u>168</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			CARBON INVENTORY: ENDING: <u>15</u> FT. OUT <u>34</u> IN OUT BEGINNING: <u>15</u> FT. OUT <u>22</u> IN OUT RECEIVED: <u>0.00</u> TONS EOM OUT: <u>17.83</u>
TOTAL STEAM FLOW: <u>906.0</u> KLB TOTAL REFUSE PR. <u>119.0</u> TONS	GROSS REFUSE REC: <u>317.31</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>19.55</u> TONS ✓ TOTAL REFUSE REC: <u>297.76</u> TONS ✓		
WELL WATER USE: ENDING: <u>413541000</u> GAL BEGINNING: <u>413364000</u> GAL TOTAL USED: <u>177000</u> GAL	EST PIT INVENTORY: <u>2,800.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>113.98</u>	MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>0.0</u> % UNIT 1 % MCR: <u>0.0</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>422.5</u>	UNIT 2 AVAILABILITY: <u>62.6</u> % UNIT 2 % MCR: <u>58.6</u> % LB STEAM/GROSS KW <u>15.7</u> LB LIME/TON PR.: <u>5.3</u>	TG AVAILABILITY: <u>61.3</u> % TG % MCR: <u>15.3</u> % GROSS KW/TON PR. <u>484.0</u> TOT STM TO T/G: <u>784.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler off line for scheduled outage ,#2 boiler off line outage

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE APRIL 10 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>0.0</u> KLB	STEAM PRODUCED: <u>0.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>0.0</u> KLB	FEEDWATER USED: <u>0.0</u> KLB	ENDING: <u>8347.0</u> WH TOT	BEGINNING: <u>174084</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8347.0</u> WH TOT	ENDING: <u>174064</u> CU FT
BLOWDOWN: <u>0</u> KLB	BLOWDOWN: <u>0</u> KLB	TOTAL: <u>0.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>ERR</u> %	BLOWDOWN: <u>ERR</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4323080</u> JEM TOT	ENDING: <u>3.5</u> FT/IN OUT
ENDING: <u>73975.5</u> HRS	ENDING: <u>73016.3</u> HRS	BEGINNING: <u>4323080</u> JEM TOT	BEGINNING: <u>3.5</u> FT/IN OUT
BEGINNING: <u>73975.5</u> HRS	BEGINNING: <u>73016.3</u> HRS	TOTAL: <u>0.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>0.0</u> HRS	TOTAL: <u>0.0</u> HRS	UTILITY IN:	EOM OUT: <u>3.42</u>
BOILER RUN TIME: <u>0.0</u> HRS	BOILER RUN TIME: <u>0.0</u> HRS	ENDING: <u>2634620</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>ERR</u> KLB/HR	AVG. STEAM FLOW: <u>ERR</u> KLB/HR	BEGINNING: <u>2611610</u> JEM TOT	USAGE UNIT #1: <u>0</u> LBS
APPROX REF PROC: <u>0.0</u> TONS	APPROX REF PROC: <u>0.0</u> TONS	TOTAL: <u>23.0</u> MWH	USAGE UNIT #2: <u>0</u> LBS
REFUSE PROCESSED: <u>0.0</u> TONS	REFUSE PROCESSED: <u>0.0</u> TONS	GENERATOR RUN TIME: <u>0.0</u> HRS	DAILY TOTAL: <u>0</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>23.0</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>ERR</u>	ENDING: <u>15</u> FT. OUT <u>31</u> IN OUT
TOTAL STEAM FLOW: <u>0.0</u> KLB	GROSS REFUSE REC: <u>66.00</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>34</u> IN OUT
TOTAL REFUSE PR. <u>0.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>17.58</u>
	TOTAL REFUSE REC: <u>66.00</u> TONS <i>66.23</i>		
WELL WATER USE:	EST PIT INVENTORY: <u>2,866.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>413384000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>413153000</u> GAL		% OF REFUSE PROC: <u>ERR</u> %	
TOTAL USED: <u>211000</u> GAL			
UNIT 1 AVAILABILITY: <u>0.0</u> %	UNIT 2 AVAILABILITY: <u>0.0</u> %	TG AVAILABILITY: <u>0.0</u> %	
UNIT 1 % MCR: <u>0.0</u> %	UNIT 2 % MCR: <u>0.0</u> %	TG % MCR: <u>0.0</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>ERR</u>	GROSS KW/TON PR. <u>ERR</u>	
NET KWH/TON PR. <u>ERR</u>	LB LIME/TON PR.: <u>ERR</u>	TOT STM TO T/G: <u>0.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler off line for scheduled outage, #2 boiler off line outage

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 11 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>0.0</u> KLB	STEAM PRODUCED: <u>0.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>0.0</u> KLB	FEEDWATER USED: <u>0.0</u> KLB	ENDING: <u>8347.0</u> WH TOT	BEGINNING: <u>174064</u> CU FT
		BEGINNING: <u>8347.0</u> WH TOT	ENDING: <u>174109</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	TOTAL: <u>0.0</u> MWH	TOTAL USED: <u>45</u> CU FT
BLOWDOWN: <u>0</u> KLB	BLOWDOWN: <u>0</u> KLB		
BLOWDOWN : <u>ERR</u> %	BLOWDOWN : <u>ERR</u> %	UTILITY OUT:	PEBBLE LIME :
		ENDING: <u>4323080</u> JEM TOT	ENDING: <u>3.5</u> FT/IN OUT
GRATE RUN TIME:	GRATE RUN TIME:	BEGINNING: <u>4323080</u> JEM TOT	BEGINNING: <u>3.5</u> FT/IN OUT
ENDING: <u>74071.5</u> HRS	ENDING: <u>73040.4</u> HRS	TOTAL: <u>0.0</u> MWH	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>74071.5</u> HRS	BEGINNING: <u>73040.4</u> HRS		
TOTAL: <u>0.0</u> HRS	TOTAL: <u>0.0</u> HRS		
		UTILITY IN:	EOM OUT: <u>3.42</u>
BOILER RUN TIME: <u>0.0</u> HRS	BOILER RUN TIME: <u>0.0</u> HRS	ENDING: <u>2656090</u> JEM TOT	
		BEGINNING: <u>2634620</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>ERR</u> KLB/HR	AVG. STEAM FLOW: <u>ERR</u> KLB/HR	TOTAL: <u>21.5</u> MWH	USAGE UNIT #1: <u>0</u> LBS
			USAGE UNIT #2: <u>0</u> LBS
APPROX REF PROC: <u>0.0</u> TONS	APPROX REF PROC: <u>0.0</u> TONS	GENERATOR RUN TIME: <u>0.0</u> HRS	DAILY TOTAL: <u>0</u> LBS
REFUSE PROCESSED: <u>0.0</u> TONS	REFUSE PROCESSED: <u>0.0</u> TONS	IN PLANT USE: <u>21.5</u> MWH	
		KWH/TON: <u>ERR</u>	CARBON INVENTORY:
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			ENDING: <u>15</u> FT. OUT <u>31</u> IN OUT
			BEGINNING: <u>15</u> FT. OUT <u>34</u> IN OUT
TOTAL STEAM FLOW: <u>0.0</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
TOTAL REFUSE PR. <u>0.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		
	FERROUS HAULED: <u>0.00</u> TONS ✓		
	TOTAL REFUSE REC: <u>0.00</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>2,866.0</u> TONS	MEDICAL WASTE :	EOM OUT: <u>17.58</u>
ENDING: <u>413774000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>413655000</u> GAL		% OF REFUSE PROC: <u>ERR</u> %	
TOTAL USED: <u>119000</u> GAL			
UNIT 1 AVAILABILITY: <u>0.0</u> %	UNIT 2 AVAILABILITY: <u>0.0</u> %	TG AVAILABILITY: <u>0.0</u> %	
UNIT 1 % MCR: <u>0.0</u> %	UNIT 2 % MCR: <u>0.0</u> %	TG % MCR: <u>0.0</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>ERR</u>	GROSS KW/TON PR. <u>ERR</u>	
NET KWH/TON PR. <u>ERR</u>	LB LIME/TON PR.: <u>ERR</u>	TOT STM TO T/G: <u>0.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler off line for scheduled outage ,#2 boiler off line outage

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 12 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>0.0</u> KLB	STEAM PRODUCED: <u>1054.6</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>0.0</u> KLB	FEEDWATER USED: <u>1067.3</u> KLB	ENDING: <u>8347.0</u> WH TOT	BEGINNING: <u>174109</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8347.0</u> WH TOT	ENDING: <u>174839</u> CU FT
BLOWDOWN: <u>0</u> KLB	BLOWDOWN: <u>13</u> KLB	TOTAL: <u>0.0</u> MWH	TOTAL USED: <u>730</u> CU FT
BLOWDOWN : <u>ERR</u> %	BLOWDOWN : <u>1.2</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4323080</u> JEM TOT	ENDING: <u>3.5</u> FT/IN OUT
ENDING: <u>74071.5</u> HRS	ENDING: <u>73064.4</u> HRS	BEGINNING: <u>4323080</u> JEM TOT	BEGINNING: <u>3.5</u> FT/IN OUT
BEGINNING: <u>74071.5</u> HRS	BEGINNING: <u>73040.4</u> HRS	TOTAL: <u>0.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>0.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>0.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>3.42</u>
AVG. STEAM FLOW: <u>ERR</u> KLB/HR	AVG. STEAM FLOW: <u>43.9</u> KLB/HR	ENDING: <u>2686270</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>0.0</u> TONS	APPROX REF PROC: <u>142.5</u> TONS	BEGINNING: <u>2656090</u> JEM TOT	USAGE UNIT #1: <u>0</u> LBS
REFUSE PROCESSED: <u>0.0</u> TONS	REFUSE PROCESSED: <u>175.8</u> TONS	TOTAL: <u>30.2</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>0.0</u> HRS	DAILY TOTAL: <u>269</u> LBS
		IN PLANT USE: <u>30.2</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>211.8</u>	ENDING: <u>15</u> FT. OUT <u>16</u> IN OUT
TOTAL STEAM FLOW: <u>1054.6</u> KLB	GROSS REFUSE REC: <u>356.84</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>34</u> IN OUT
TOTAL REFUSE PR. <u>142.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>16.33</u>
ENDING: <u>414010000</u> GAL	TOTAL REFUSE REC: <u>356.84</u> TONS ✓	MEDICAL WASTE :	
BEGINNING: <u>413774000</u> GAL	EST PIT INVENTORY: <u>3,053.0</u> TONS	PROCESSED: <u>0.00</u> TONS	
TOTAL USED: <u>236000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>0.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>0.0</u> %	
UNIT 1 % MCR: <u>0.0</u> %	UNIT 2 % MCR: <u>68.2</u> %	TG % MCR: <u>0.0</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>ERR</u>	GROSS KW/TON PR. <u>0.0</u>	
NET KWH/TON PR. <u>0.0</u>	LB LIME/TON PR.: <u>0.0</u>	TOT STM TO T/G: <u>774.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler off line for scheduled outage

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 13 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1142.9</u> KLB	STEAM PRODUCED: <u>1424.9</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1359.8</u> KLB	FEEDWATER USED: <u>1476.3</u> KLB	ENDING: <u>8348.0</u> WH TOT	BEGINNING: <u>174839</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8347.0</u> WH TOT	ENDING: <u>175529</u> CU FT
BLOWDOWN: <u>217</u> KLB	BLOWDOWN: <u>51</u> KLB	TOTAL: <u>28.8</u> MWH	TOTAL USED: <u>690</u> CU FT
BLOWDOWN: <u>16.0</u> %	BLOWDOWN: <u>3.5</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4354550</u> JEM TOT	ENDING: <u>4.6</u> FT/IN OUT
ENDING: <u>74117.5</u> HRS	ENDING: <u>73088.4</u> HRS	BEGINNING: <u>4323080</u> JEM TOT	BEGINNING: <u>3.5</u> FT/IN OUT
BEGINNING: <u>74097.5</u> HRS	BEGINNING: <u>73064.4</u> HRS	TOTAL: <u>31.5</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>20.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>4.50</u>
BOILER RUN TIME: <u>20.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>57.1</u> KLB/HR	AVG. STEAM FLOW: <u>59.4</u> KLB/HR	BEGINNING: <u>2686270</u> JEM TOT	USAGE UNIT #1: <u>224</u> LBS
APPROX REF PROC: <u>127.8</u> TONS	APPROX REF PROC: <u>202.8</u> TONS	TOTAL: <u>36.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>190.5</u> TONS	REFUSE PROCESSED: <u>237.5</u> TONS	GENERATOR RUN TIME: <u>3.2</u> HRS	DAILY TOTAL: <u>493</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>33.3</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>99.8</u>	ENDING: <u>14</u> FT. OUT <u>65</u> IN OUT
TOTAL STEAM FLOW: <u>2567.8</u> KLB	GROSS REFUSE REC: <u>346.00</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>18</u> IN OUT
TOTAL REFUSE PR. <u>333.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>19.42</u>
	TOTAL REFUSE REC: <u>346.00</u> TONS <u>342.97</u>		
WELL WATER USE:	EST PIT INVENTORY: <u>3,228.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>414389000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	PROCESSED: <u>3.03</u> TONS	
BEGINNING: <u>414010000</u> GAL		% OF REFUSE PROC: <u>0.91</u> %	
TOTAL USED: <u>379000</u> GAL			
UNIT 1 AVAILABILITY: <u>83.3</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>13.3</u> %	
UNIT 1 % MCR: <u>73.9</u> %	UNIT 2 % MCR: <u>92.2</u> %	TG % MCR: <u>7.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>89.2</u>	GROSS KW/TON PR. <u>86.3</u>	
NET KWH/TON PR. <u>94.3</u>	LB LIME/TON PR.: <u>10.4</u>	TOT STM TO T/G: <u>2,236.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 14 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1433.9</u> KLB FEEDWATER USED: <u>1502.6</u> KLB	STEAM PRODUCED: <u>1540.1</u> KLB FEEDWATER USED: <u>1620.1</u> KLB	GENERATOR OUT: ENDING: <u>8358.0</u> WH TOT BEGINNING: <u>8348.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>175529</u> CU FT ENDING: <u>175529</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>69</u> KLB BLOWDOWN : <u>4.6</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>80</u> KLB BLOWDOWN : <u>4.9</u> %	UTILITY OUT: ENDING: <u>4597940</u> JEM TOT BEGINNING: <u>4354550</u> JEM TOT TOTAL: <u>243.4</u> MWH	PEBBLE LIME : ENDING: <u>6.4</u> FT/IN OUT BEGINNING: <u>4.6</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>74141.5</u> HRS BEGINNING: <u>74117.5</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>73112.4</u> HRS BEGINNING: <u>73088.4</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2722250</u> JEM TOT BEGINNING: <u>2722250</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>6.33</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>59.7</u> KLB/HR APPROX REF PROC: <u>233.4</u> TONS	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>64.2</u> KLB/HR APPROX REF PROC: <u>232.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>44.6</u> MWH KWH/TON: <u>94.9</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
REFUSE PROCESSED: <u>239.0</u> TONS	REFUSE PROCESSED: <u>256.7</u> TONS		CARBON INVENTORY: ENDING: <u>13</u> FT. OUT <u>97</u> IN OUT BEGINNING: <u>14</u> FT. OUT <u>34</u> IN OUT RECEIVED: <u>0.00</u> TONS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			EOM OUT: <u>21.08</u>
TOTAL STEAM FLOW: <u>2974.0</u> KLB TOTAL REFUSE PR. <u>470.0</u> TONS	GROSS REFUSE REC: <u>194.83</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>194.83</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>4.57</u> TONS % OF REFUSE PROC: <u>0.97</u> %	
WELL WATER USE: ENDING: <u>414723000</u> GAL BEGINNING: <u>414389000</u> GAL TOTAL USED: <u>334000</u> GAL	EST PIT INVENTORY: <u>2,995.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>101.87</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>92.8</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>517.9</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>99.6</u> % LB STEAM/GROSS KW <u>10.3</u> LB LIME/TON PR.: <u>12.0</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>612.8</u> TOT STM TO T/G: <u>2,895.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE April 15, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1472.9</u> KLB	STEAM PRODUCED: <u>1553.2</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1543.4</u> KLB	FEEDWATER USED: <u>1642.7</u> KLB	ENDING: <u>8369.0</u> WH TOT	BEGINNING: <u>175529</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8358.0</u> WH TOT	ENDING: <u>175645</u> CU FT
BLOWDOWN: <u>70</u> KLB	BLOWDOWN: <u>90</u> KLB	TOTAL: <u>316.8</u> MWH	TOTAL USED: <u>116</u> CU FT
BLOWDOWN: <u>4.6</u> %	BLOWDOWN: <u>5.4</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4843340</u> JEM TOT	ENDING: <u>6.5</u> FT/IN OUT
ENDING: <u>74165.0</u> HRS	ENDING: <u>73138.0</u> HRS	BEGINNING: <u>4597940</u> JEM TOT	BEGINNING: <u>6.4</u> FT/IN OUT
BEGINNING: <u>74141.5</u> HRS	BEGINNING: <u>73112.4</u> HRS	TOTAL: <u>245.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>23.5</u> HRS	TOTAL: <u>23.6</u> HRS	UTILITY IN:	EOM OUT: <u>6.42</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>61.4</u> KLB/HR	AVG. STEAM FLOW: <u>64.7</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>207.0</u> TONS	APPROX REF PROC: <u>214.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>245.5</u> TONS	REFUSE PROCESSED: <u>258.9</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>71.4</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>161.7</u>	ENDING: <u>14</u> FT. OUT <u>46</u> IN OUT
TOTAL STEAM FLOW: <u>3026.1</u> KLB	GROSS REFUSE REC: <u>256.57</u> TONS		BEGINNING: <u>13</u> FT. OUT <u>97</u> IN OUT
TOTAL REFUSE PR. <u>441.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>17.83</u>
	TOTAL REFUSE REC: <u>256.57</u> TONS ✓		
WELL WATER USE: <u>5045.4</u>	EST PIT INVENTORY: <u>2,509.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>415067000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>20.69</u> TONS	
BEGINNING: <u>414723000</u> GAL		% OF REFUSE PROC: <u>4.68</u> %	
TOTAL USED: <u>344000</u> GAL			
	<u>153.96</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>95.3</u> %	UNIT 2 % MCR: <u>100.5</u> %	TG % MCR: <u>84.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.6</u>	GROSS KW/TON PR. <u>717.2</u>	
NET KWH/TON PR. <u>555.6</u>	LB LIME/TON PR.: <u>0.7</u>	TOT STM TO T/G: <u>2,965.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE April 16, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1469.0</u> KLB	STEAM PRODUCED: <u>1366.3</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1539.7</u> KLB	FEEDWATER USED: <u>1446.9</u> KLB	ENDING: <u>6378.0</u> WH TOT	BEGINNING: <u>175645</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8369.0</u> WH TOT	ENDING: <u>175758</u> CU FT
BLOWDOWN: <u>71</u> KLB	BLOWDOWN: <u>81</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>113</u> CU FT
BLOWDOWN %: <u>4.6</u> %	BLOWDOWN %: <u>5.6</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>5070540</u> JEM TOT	ENDING: <u>6.9</u> FT/IN OUT
ENDING: <u>74188.9</u> HRS	ENDING: <u>73157.7</u> HRS	BEGINNING: <u>4843346</u> JEM TOT	BEGINNING: <u>6.5</u> FT/IN OUT
BEGINNING: <u>74165.0</u> HRS	BEGINNING: <u>73136.0</u> HRS	TOTAL: <u>227.2</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>23.9</u> HRS	TOTAL: <u>21.7</u> HRS	UTILITY IN:	EOM OUT: <u>6.75</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>21.7</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>61.2</u> KLB/HR	AVG. STEAM FLOW: <u>63.0</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>224.0</u> TONS	APPROX REF PROC: <u>205.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>243</u> LBS
REFUSE PROCESSED: <u>244.8</u> TONS	REFUSE PROCESSED: <u>227.7</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>512</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>32.0</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2835.3</u> KLB	GROSS REFUSE REC: <u>301.07</u> TONS	KWH/TON: <u>73.1</u>	ENDING: <u>14</u> FT. OUT <u>6</u> IN OUT
TOTAL REFUSE PR. <u>437.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>14</u> FT. OUT <u>46</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
ENDING: <u>415405000</u> GAL	TOTAL REFUSE REC: <u>301.07</u> TONS <u>302.60</u>	MEDICAL WASTE:	EOM OUT: <u>14.50</u>
BEGINNING: <u>415067000</u> GAL	EST PIT INVENTORY: <u>2,684.0</u> TONS	PROCESSED: <u>8.49</u> TONS	
TOTAL USED: <u>338000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.94</u> %	
	<u>72.21</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>90.4</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>95.0</u> %	UNIT 2 % MCR: <u>88.4</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.9</u>	GROSS KW/TON PR. <u>592.5</u>	
NET KWH/TON PR. <u>519.3</u>	LB LIME/TON PR.: <u>2.9</u>	TOT STM TO T/G: <u>2,743.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 17, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1478.4</u> KLB FEEDWATER USED: <u>1545.8</u> KLB	STEAM PRODUCED: <u>1521.1</u> KLB FEEDWATER USED: <u>1608.4</u> KLB	GENERATOR OUT: ENDING: <u>8389.0</u> WH TOT BEGINNING: <u>8378.0</u> WH TOT TOTAL: <u>316.8</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>175758</u> CU FT ENDING: <u>175758</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>69</u> KLB BLOWDOWN: <u>4.5</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>87</u> KLB BLOWDOWN: <u>5.4</u> %	UTILITY OUT: ENDING: <u>5319720</u> JEM TOT BEGINNING: <u>5070540</u> JEM TOT TOTAL: <u>249.2</u> MWH	PEBBLE LIME : ENDING: <u>7.5</u> FT/IN OUT BEGINNING: <u>6.9</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>74212.9</u> HRS BEGINNING: <u>74188.9</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>73181.6</u> HRS BEGINNING: <u>73157.7</u> HRS TOTAL: <u>23.9</u> HRS	UTILITY IN: ENDING: <u>2722250</u> JEM TOT BEGINNING: <u>2722250</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>7.42</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>61.5</u> KLB/HR	AVG. STEAM FLOW: <u>63.4</u> KLB/HR	IN PLANT USE: <u>67.6</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>270.0</u> TONS	APPROX REF PROC: <u>278.0</u> TONS	KWH/TON: <u>134.1</u>	CARBON INVENTORY: ENDING: <u>13</u> FT. OUT <u>39</u> IN OUT BEGINNING: <u>14</u> FT. OUT <u>6</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>246.1</u> TONS	REFUSE PROCESSED: <u>253.5</u> TONS		EOM OUT: <u>16.25</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2997.5</u> KLB TOTAL REFUSE PR. <u>504.1</u> TONS	GROSS REFUSE REC: <u>63.94</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>12.59</u> TONS ✓ TOTAL REFUSE REC: <u>51.35</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>4.53</u> TONS % OF REFUSE PROC: <u>0.90</u> %	
WELL WATER USE: ENDING: <u>415728000</u> GAL BEGINNING: <u>415405000</u> GAL TOTAL USED: <u>323000</u> GAL	EST PIT INVENTORY: <u>2,275.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>126.05</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>95.5</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>494.3</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>98.4</u> % LB STEAM/GROSS KW <u>9.5</u> LB LIME/TON PR.: <u>3.7</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>84.1</u> % GROSS KW/TON PR. <u>628.4</u> TOT STM TO T/G: <u>2,969.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE April 18, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1401.8</u> KLB	STEAM PRODUCED: <u>1387.9</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1468.1</u> KLB	FEEDWATER USED: <u>1467.0</u> KLB	ENDING: <u>8398.0</u> WH TOT	BEGINNING: <u>175758</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8389.0</u> WH TOT	ENDING: <u>175829</u> CU FT
BLOWDOWN: <u>66</u> KLB	BLOWDOWN: <u>79</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>71</u> CU FT
BLOWDOWN: <u>4.5</u> %	BLOWDOWN: <u>5.4</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>5547390</u> JEM TOT	ENDING: <u>8.4</u> FT/IN OUT
ENDING: <u>74236.4</u> HRS	ENDING: <u>73205.6</u> HRS	BEGINNING: <u>5319720</u> JEM TOT	BEGINNING: <u>7.5</u> FT/IN OUT
BEGINNING: <u>74212.9</u> HRS	BEGINNING: <u>73181.6</u> HRS	TOTAL: <u>227.7</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>23.5</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>8.33</u>
AVG. STEAM FLOW: <u>58.4</u> KLB/HR	AVG. STEAM FLOW: <u>57.8</u> KLB/HR	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>273.0</u> TONS	APPROX REF PROC: <u>262.0</u> TONS	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>233.6</u> TONS	REFUSE PROCESSED: <u>231.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2789.7</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS	IN PLANT USE: <u>31.5</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>484.9</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>67.8</u>	ENDING: <u>13</u> FT. OUT <u>74</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>13</u> FT. OUT <u>39</u> IN OUT
ENDING: <u>416057000</u> GAL	TOTAL REFUSE REC: <u>0.00</u> TONS ✓	MEDICAL WASTE:	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>415728000</u> GAL	EST PIT INVENTORY: <u>1,634.0</u> TONS	PROCESSED: <u>0.00</u> TONS	EOM OUT: <u>19.17</u>
TOTAL USED: <u>329000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>90.7</u> %	UNIT 2 % MCR: <u>89.8</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.8</u>	GROSS KW/TON PR. <u>557.5</u>	
NET KWH/TON PR. <u>489.7</u>	LB LIME/TON PR.: <u>8.1</u>	TOT STM TO T/G: <u>2,727.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 19, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>971.0</u> KLB	STEAM PRODUCED: <u>1409.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>932.0</u> KLB	FEEDWATER USED: <u>1442.0</u> KLB	ENDING: <u>8406.0</u> WH TOT	BEGINNING: <u>175829</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8396.0</u> WH TOT	ENDING: <u>175835</u> CU FT
BLOWDOWN: <u>-39</u> KLB	BLOWDOWN: <u>33</u> KLB	TOTAL: <u>230.4</u> MWH	TOTAL USED: <u>8</u> CU FT
BLOWDOWN: <u>-4.2</u> %	BLOWDOWN: <u>2.3</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>5723790</u> JEM TOT	ENDING: <u>5.3</u> FT/IN OUT
ENDING: <u>74280.4</u> HRS	ENDING: <u>73229.6</u> HRS	BEGINNING: <u>5547390</u> JEM TOT	BEGINNING: <u>8.4</u> FT/IN OUT
BEGINNING: <u>74236.4</u> HRS	BEGINNING: <u>73205.6</u> HRS	TOTAL: <u>176.4</u> MWH	RECEIVED: <u>24.37</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>5.21</u>
BOILER RUN TIME: <u>15.1</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>64.3</u> KLB/HR	AVG. STEAM FLOW: <u>58.7</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>169</u> LBS
APPROX REF PROC: <u>147.0</u> TONS	APPROX REF PROC: <u>242.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>161.8</u> TONS	REFUSE PROCESSED: <u>234.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>438</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>54.0</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2380.0</u> KLB	GROSS REFUSE REC: <u>756.71</u> TONS	KWH/TON: <u>136.1</u>	ENDING: <u>13</u> FT. OUT <u>35</u> IN OUT
TOTAL REFUSE PR. <u>396.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>13</u> FT. OUT <u>74</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
ENDING: <u>416360000</u> GAL	TOTAL REFUSE REC: <u>756.71</u> TONS <u>755.51</u>	MEDICAL WASTE:	EOM OUT: <u>15.92</u>
BEGINNING: <u>416057000</u> GAL	EST PIT INVENTORY: <u>2,334.0</u> TONS	PROCESSED: <u>7.71</u> TONS	
TOTAL USED: <u>303000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.94</u> %	
	<u>165.74</u>		
UNIT 1 AVAILABILITY: <u>62.9</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>62.8</u> %	UNIT 2 % MCR: <u>91.2</u> %	TG % MCR: <u>61.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.3</u>	GROSS KW/TON PR. <u>580.8</u>	
NET KWH/TON PR. <u>444.7</u>	LB LIME/TON PR.: <u>97.9</u>	TOT STM TO T/G: <u>2,130.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler due ruptured tube in upper section of economizer section 8 hours & 53 minutes.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 20, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>0.0</u> KLB	STEAM PRODUCED: <u>1557.6</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>0.0</u> KLB	FEEDWATER USED: <u>1584.0</u> KLB	ENDING: <u>8411.0</u> WH TOT	BEGINNING: <u>175835</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8406.0</u> WH TOT	ENDING: <u>175835</u> CU FT
BLOWDOWN: <u>0</u> KLB	BLOWDOWN: <u>26</u> KLB	TOTAL: <u>144.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN : <u>ERR</u> %	BLOWDOWN : <u>1.7</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>5818950</u> JEM TOT	ENDING: <u>6.6</u> FT/IN OUT
ENDING: <u>74284.4</u> HRS	ENDING: <u>73253.4</u> HRS	BEGINNING: <u>5723790</u> JEM TOT	BEGINNING: <u>5.3</u> FT/IN OUT
BEGINNING: <u>74260.4</u> HRS	BEGINNING: <u>73229.6</u> HRS	TOTAL: <u>95.2</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.8</u> HRS		
BOILER RUN TIME: <u>0.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>6.48</u>
AVG. STEAM FLOW: <u>ERR</u> KLB/HR	AVG. STEAM FLOW: <u>64.9</u> KLB/HR	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>0.0</u> TONS	APPROX REF PROC: <u>254.0</u> TONS	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>0</u> LBS
REFUSE PROCESSED: <u>0.0</u> TONS	REFUSE PROCESSED: <u>259.6</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>269</u> LBS
TOTAL STEAM FLOW: <u>1557.6</u> KLB	GROSS REFUSE REC: <u>634.90</u> TONS	IN PLANT USE: <u>48.8</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>254.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>192.3</u>	ENDING: <u>13</u> FT. OUT <u>0</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>13</u> FT. OUT <u>35</u> IN OUT
ENDING: <u>419660000</u> GAL	TOTAL REFUSE REC: <u>634.90</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>416360000</u> GAL	EST PIT INVENTORY: <u>2,772.0</u> TONS	MEDICAL WASTE :	EOM OUT: <u>13.00</u>
TOTAL USED: <u>3300000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.00</u> TONS	
	<u>104.04</u>	% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>0.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>0.0</u> %	UNIT 2 % MCR: <u>100.8</u> %	TG % MCR: <u>38.2</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.8</u>	GROSS KW/TON PR. <u>566.9</u>	
NET KWH/TON PR. <u>374.6</u>	LB LIME/TON PR.: <u>15.8</u>	TOT STM TO T/G: <u>1,293.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler off line to repair ruptured tube in economizer 24 hours.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 21, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1049.2</u> KLB	STEAM PRODUCED: <u>1542.4</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1071.4</u> KLB	FEEDWATER USED: <u>1576.0</u> KLB	ENDING: <u>8419.0</u> WH TOT	BEGINNING: <u>175835</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8411.0</u> WH TOT	ENDING: <u>176133</u> CU FT
BLOWDOWN: <u>22</u> KLB	BLOWDOWN: <u>34</u> KLB	TOTAL: <u>230.4</u> MWH	TOTAL USED: <u>298</u> CU FT
BLOWDOWN: <u>2.1</u> %	BLOWDOWN: <u>2.1</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>6014810</u> JEM TOT	ENDING: <u>6.8</u> FT/IN OUT
ENDING: <u>74300.8</u> HRS	ENDING: <u>73277.4</u> HRS	BEGINNING: <u>5818950</u> JEM TOT	BEGINNING: <u>6.6</u> FT/IN OUT
BEGINNING: <u>74284.4</u> HRS	BEGINNING: <u>73253.4</u> HRS	TOTAL: <u>195.9</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>16.4</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>6.67</u>
BOILER RUN TIME: <u>17.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>61.7</u> KLB/HR	AVG. STEAM FLOW: <u>64.3</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>190</u> LBS
APPROX REF PROC: <u>134.0</u> TONS	APPROX REF PROC: <u>212.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>174.9</u> TONS	REFUSE PROCESSED: <u>257.1</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>459</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>34.5</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2591.6</u> KLB	GROSS REFUSE REC: <u>565.55</u> TONS	KWH/TON: <u>97.2</u>	ENDING: <u>12</u> FT. OUT <u>98</u> IN OUT
TOTAL REFUSE PR. <u>355.3</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>13</u> FT. OUT <u>0</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>565.55</u> TONS ✓		EOM OUT: <u>20.17</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,800.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>416895000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>9.27</u> TONS	
BEGINNING: <u>416690000</u> GAL	<u>53.26</u>	% OF REFUSE PROC: <u>2.61</u> %	
TOTAL USED: <u>205000</u> GAL			
UNIT 1 AVAILABILITY: <u>70.8</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>67.9</u> %	UNIT 2 % MCR: <u>99.8</u> %	TG % MCR: <u>61.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>11.2</u>	GROSS KW/TON PR. <u>648.5</u>	
NET KWH/TON PR. <u>551.3</u>	LB LIME/TON PR.: <u>1.8</u>	TOT STM TO T/G: <u>2,356.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 boiler off line 7 hours to repair economizer rupture tube leaks.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE April 22, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1362.2</u> KLB	STEAM PRODUCED: <u>1518.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1421.3</u> KLB	FEEDWATER USED: <u>1553.9</u> KLB	ENDING: <u>8429.0</u> WH TOT	BEGINNING: <u>176133</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8419.0</u> WH TOT	ENDING: <u>176133</u> CU FT
BLOWDOWN: <u>59</u> KLB	BLOWDOWN: <u>36</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>4.2</u> %	BLOWDOWN: <u>2.3</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>6251300</u> JEM TOT	ENDING: <u>7.0</u> FT/IN OUT
ENDING: <u>74323.7</u> HRS	ENDING: <u>73301.2</u> HRS	BEGINNING: <u>6014810</u> JEM TOT	BEGINNING: <u>6.8</u> FT/IN OUT
BEGINNING: <u>74300.8</u> HRS	BEGINNING: <u>73277.4</u> HRS	TOTAL: <u>236.5</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>22.9</u> HRS	TOTAL: <u>23.8</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>7.00</u>
AVG. STEAM FLOW: <u>56.8</u> KLB/HR	AVG. STEAM FLOW: <u>63.2</u> KLB/HR	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>200.0</u> TONS	APPROX REF PROC: <u>220.0</u> TONS	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>227.0</u> TONS	REFUSE PROCESSED: <u>253.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2880.2</u> KLB	GROSS REFUSE REC: <u>184.97</u> TONS	IN PLANT USE: <u>51.5</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>421.9</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>122.1</u>	ENDING: <u>12</u> FT. OUT <u>73</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS <i>11.86</i>		BEGINNING: <u>12</u> FT. OUT <u>98</u> IN OUT
	TOTAL REFUSE REC: <u>184.97</u> TONS <i>173.11</i>		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	EST PIT INVENTORY: <u>2,397.0</u> TONS	MEDICAL WASTE:	EOM OUT: <u>18.08</u>
ENDING: <u>417122000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>1.87</u> TONS	
BEGINNING: <u>416895000</u> GAL		% OF REFUSE PROC: <u>0.44</u> %	
TOTAL USED: <u>227000</u> GAL	<i>229.30</i>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>88.1</u> %	UNIT 2 % MCR: <u>98.2</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.0</u>	GROSS KW/TON PR. <u>682.7</u>	
NET KWH/TON PR. <u>560.6</u>	LB LIME/TON PR.: <u>1.5</u>	TOT STM TO T/G: <u>2,838.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE April 23, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1144.0</u> KLB FEEDWATER USED: <u>1186.9</u> KLB	STEAM PRODUCED: <u>1130.3</u> KLB FEEDWATER USED: <u>1162.4</u> KLB	GENERATOR OUT: ENDING: <u>8436.0</u> WH TOT BEGINNING: <u>8429.0</u> WH TOT TOTAL: <u>201.6</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>176133</u> CU FT ENDING: <u>176209</u> CU FT TOTAL USED: <u>76</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>43</u> KLB BLOWDOWN: <u>3.6</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>32</u> KLB BLOWDOWN: <u>2.8</u> %	UTILITY OUT: ENDING: <u>6416850</u> JEM TOT BEGINNING: <u>6251300</u> JEM TOT TOTAL: <u>165.6</u> MWH	PEBBLE LIME : ENDING: <u>8.1</u> FT/IN OUT BEGINNING: <u>7.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>74354.8</u> HRS BEGINNING: <u>74330.8</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>73325.1</u> HRS BEGINNING: <u>73301.2</u> HRS TOTAL: <u>23.9</u> HRS	UTILITY IN: ENDING: <u>2722250</u> JEM TOT BEGINNING: <u>2722250</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>8.08</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>47.7</u> KLB/HR APPROX REF PROC: <u>189.0</u> TONS REFUSE PROCESSED: <u>190.7</u> TONS	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>47.1</u> KLB/HR APPROX REF PROC: <u>190.0</u> TONS REFUSE PROCESSED: <u>188.4</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>36.0</u> MWH KWH/TON: <u>95.1</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			CARBON INVENTORY: ENDING: <u>12</u> FT. OUT <u>5</u> IN OUT BEGINNING: <u>12</u> FT. OUT <u>73</u> IN OUT RECEIVED: <u>0.00</u> TONS EOM OUT: <u>12.42</u>
TOTAL STEAM FLOW: <u>2274.3</u> KLB TOTAL REFUSE PR. <u>379.0</u> TONS	GROSS REFUSE REC: <u>59.78</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>13.29</u> TONS ✓ TOTAL REFUSE REC: <u>46.49</u> TONS <u>24.44</u>	MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	
WELL WATER USE: ENDING: <u>417424000</u> GAL BEGINNING: <u>417122000</u> GAL TOTAL USED: <u>302000</u> GAL	EST PIT INVENTORY: <u>1,808.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>57.43</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>74.0</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>436.8</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>73.1</u> % LB STEAM/GROSS KW <u>11.3</u> LB LIME/TON PR.: <u>9.1</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>53.5</u> % GROSS KW/TON PR. <u>531.9</u> TOT STM TO T/G: <u>2,061.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE APRIL 24, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1180.8</u> KLB	STEAM PRODUCED: <u>1259.1</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1222.8</u> KLB	FEEDWATER USED: <u>1292.9</u> KLB	ENDING: <u>8444.0</u> WH TOT	BEGINNING: <u>176209</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8436.0</u> WH TOT	ENDING: <u>176682</u> CU FT
BLOWDOWN: <u>42</u> KLB	BLOWDOWN: <u>34</u> KLB	TOTAL: <u>230.4</u> MWH	TOTAL USED: <u>473</u> CU FT
BLOWDOWN : <u>3.4</u> %	BLOWDOWN : <u>2.6</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>6601130</u> JEM TOT	ENDING: <u>8.3</u> FT/IN OUT
ENDING: <u>74369.3</u> HRS	ENDING: <u>73349.0</u> HRS	BEGINNING: <u>6416850</u> JEM TOT	BEGINNING: <u>8.1</u> FT/IN OUT
BEGINNING: <u>74354.8</u> HRS	BEGINNING: <u>73325.1</u> HRS	TOTAL: <u>184.3</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>14.5</u> HRS	TOTAL: <u>23.9</u> HRS	UTILITY IN:	EOM OUT: <u>8.21</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>49.2</u> KLB/HR	AVG. STEAM FLOW: <u>52.5</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>210.0</u> TONS	APPROX REF PROC: <u>207.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>196.8</u> TONS	REFUSE PROCESSED: <u>209.9</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>46.1</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2439.9</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS	KWH/TON: <u>113.4</u>	ENDING: <u>11</u> FT. OUT <u>85</u> IN OUT
TOTAL REFUSE PR. <u>406.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>12</u> FT. OUT <u>5</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓	MEDICAL WASTE :	RECEIVED: <u>0.00</u> TONS
ENDING: <u>417713000</u> GAL	TOTAL REFUSE REC: <u>0.00</u> TONS ✓	PROCESSED: <u>0.00</u> TONS	EOM OUT: <u>18.08</u>
BEGINNING: <u>417424000</u> GAL	EST PIT INVENTORY: <u>1,108.0</u> TONS	% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>289000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>76.4</u> %	UNIT 2 % MCR: <u>81.5</u> %	TG % MCR: <u>61.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.6</u>	GROSS KW/TON PR. <u>566.6</u>	
NET KWH/TON PR. <u>453.2</u>	LB LIME/TON PR.: <u>1.2</u>	TOT STM TO T/G: <u>2,267.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE APRIL 25, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1283.5</u> KLB	STEAM PRODUCED: <u>1323.5</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1326.5</u> KLB	FEEDWATER USED: <u>1354.1</u> KLB	ENDING: <u>8453.0</u> WH TOT	BEGINNING: <u>176682</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8444.0</u> WH TOT	ENDING: <u>177641</u> CU FT
BLOWDOWN: <u>43</u> KLB	BLOWDOWN: <u>31</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>959</u> CU FT
BLOWDOWN: <u>3.2</u> %	BLOWDOWN: <u>2.3</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>6809930</u> JEM TOT	ENDING: <u>9.8</u> FT/IN OUT
ENDING: <u>74393.3</u> HRS	ENDING: <u>73372.9</u> HRS	BEGINNING: <u>6601130</u> JEM TOT	BEGINNING: <u>8.3</u> FT/IN OUT
BEGINNING: <u>74369.3</u> HRS	BEGINNING: <u>73349.0</u> HRS	TOTAL: <u>208.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.9</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.67</u>
AVG. STEAM FLOW: <u>53.5</u> KLB/HR	AVG. STEAM FLOW: <u>55.1</u> KLB/HR	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>192.0</u> TONS	APPROX REF PROC: <u>201.0</u> TONS	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>213.9</u> TONS	REFUSE PROCESSED: <u>220.6</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2607.0</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS	IN PLANT USE: <u>50.4</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>393.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>128.2</u>	ENDING: <u>11</u> FT. OUT <u>82</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		BEGINNING: <u>11</u> FT. OUT <u>85</u> IN OUT
ENDING: <u>418003000</u> GAL	TOTAL REFUSE REC: <u>0.00</u> TONS ✓	MEDICAL WASTE :	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>417713000</u> GAL	EST PIT INVENTORY: <u>933.0</u> TONS	PROCESSED: <u>0.00</u> TONS	EOM OUT: <u>17.83</u>
TOTAL USED: <u>290000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>83.0</u> %	UNIT 2 % MCR: <u>85.6</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.1</u>	GROSS KW/TON PR. <u>659.5</u>	
NET KWH/TON PR. <u>531.3</u>	LB LIME/TON PR.: <u>12.0</u>	TOT STM TO T/G: <u>2,595.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 26, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1255.0</u> KLB FEEDWATER USED: <u>1297.0</u> KLB	STEAM PRODUCED: <u>1289.0</u> KLB FEEDWATER USED: <u>1322.0</u> KLB	GENERATOR OUT: ENDING: <u>8461.0</u> WH TOT BEGINNING: <u>8453.0</u> WH TOT TOTAL: <u>230.4</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>177641</u> CU FT ENDING: <u>179897</u> CU FT TOTAL USED: <u>2256</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>42</u> KLB BLOWDOWN: <u>3.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>33</u> KLB BLOWDOWN: <u>2.5</u> %	UTILITY OUT: ENDING: <u>7010500</u> JEM TOT BEGINNING: <u>6809930</u> JEM TOT TOTAL: <u>200.6</u> MWH	PEBBLE LIME : ENDING: <u>12.0</u> FT/IN OUT BEGINNING: <u>9.8</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>74417.1</u> HRS BEGINNING: <u>74393.3</u> HRS TOTAL: <u>23.8</u> HRS	GRATE RUN TIME: ENDING: <u>73394.8</u> HRS BEGINNING: <u>73372.9</u> HRS TOTAL: <u>21.9</u> HRS	UTILITY IN: ENDING: <u>2722250</u> JEM TOT BEGINNING: <u>2722250</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>12.00</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>52.3</u> KLB/HR APPROX REF PROC: <u>131.0</u> TONS REFUSE PROCESSED: <u>209.2</u> TONS	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>53.7</u> KLB/HR APPROX REF PROC: <u>134.0</u> TONS REFUSE PROCESSED: <u>214.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>29.8</u> MWH KWH/TON: <u>111.5</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			CARBON INVENTORY: ENDING: <u>11</u> FT. OUT <u>75</u> IN OUT BEGINNING: <u>11</u> FT. OUT <u>82</u> IN OUT RECEIVED: <u>0.00</u> TONS
TOTAL STEAM FLOW: <u>2544.0</u> KLB TOTAL REFUSE PR. <u>267.5</u> TONS	GROSS REFUSE REC: <u>64.75</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>64.75</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>2.48</u> TONS % OF REFUSE PROC: <u>0.93</u> %	EOM OUT: <u>17.25</u>
WELL WATER USE: ENDING: <u>418291000</u> GAL BEGINNING: <u>418003000</u> GAL TOTAL USED: <u>288000</u> GAL	EST PIT INVENTORY: <u>788.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>186.78</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>81.2</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>749.9</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>83.4</u> % LB STEAM/GROSS KW <u>11.0</u> LB LIME/TON PR.: <u>25.8</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>61.1</u> % GROSS KW/TON PR. <u>861.4</u> TOT STM TO T/G: <u>2,461.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 27, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1307.0</u> KLB FEEDWATER USED: <u>1351.0</u> KLB	STEAM PRODUCED: <u>1328.0</u> KLB FEEDWATER USED: <u>1367.0</u> KLB	GENERATOR OUT: ENDING: <u>8470.0</u> WH TOT BEGINNING: <u>8461.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>179897</u> CU FT ENDING: <u>180520</u> CU FT TOTAL USED: <u>623</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>44</u> KLB BLOWDOWN : <u>3.3</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>39</u> KLB BLOWDOWN : <u>2.9</u> %	UTILITY OUT: ENDING: <u>7221610</u> JEM TOT BEGINNING: <u>7010500</u> JEM TOT TOTAL: <u>211.1</u> MWH	PEBBLE LIME : ENDING: <u>12.8</u> FT/IN OUT BEGINNING: <u>12.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>74441.1</u> HRS BEGINNING: <u>74417.1</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>73418.7</u> HRS BEGINNING: <u>73394.8</u> HRS TOTAL: <u>23.9</u> HRS	UTILITY IN: ENDING: <u>2722250</u> JEM TOT BEGINNING: <u>2722250</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>12.67</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>54.5</u> KLB/HR	AVG. STEAM FLOW: <u>55.3</u> KLB/HR	IN PLANT USE: <u>48.1</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>209.0</u> TONS	APPROX REF PROC: <u>171.4</u> TONS	KWH/TON: <u>124.7</u>	CARBON INVENTORY: ENDING: <u>11</u> FT. OUT <u>20</u> IN OUT BEGINNING: <u>11</u> FT. OUT <u>75</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>217.8</u> TONS	REFUSE PROCESSED: <u>221.3</u> TONS		EOM OUT: <u>12.67</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2635.0</u> KLB TOTAL REFUSE PR. <u>385.6</u> TONS	GROSS REFUSE REC: <u>662.63</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS TOTAL REFUSE REC: <u>662.63</u> TONS <i>656.13</i>	MEDICAL WASTE : PROCESSED: <u>5.23</u> TONS % OF REFUSE PROC: <u>1.36</u> %	
WELL WATER USE: ENDING: <u>418593000</u> GAL BEGINNING: <u>418291000</u> GAL TOTAL USED: <u>302000</u> GAL	EST PIT INVENTORY: <u>1,669.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>139.87</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>84.6</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>547.5</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>85.9</u> % LB STEAM/GROSS KW <u>10.2</u> LB LIME/TON PR.: <u>6.5</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>672.2</u> TOT STM TO T/G: <u>2,607.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 28, 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1385.0</u> KLB FEEDWATER USED: <u>1433.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>48</u> KLB BLOWDOWN: <u>3.3</u> %</p> <p>GRATE RUN TIME: ENDING: <u>74465.1</u> HRS BEGINNING: <u>74441.1</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>57.7</u> KLB/HR</p> <p>APPROX REF PROC: <u>200.0</u> TONS</p> <p>REFUSE PROCESSED: <u>230.8</u> TONS</p> <p>NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB</p> <p>TOTAL STEAM FLOW: <u>2836.0</u> KLB TOTAL REFUSE PR. <u>439.4</u> TONS</p> <p>WELL WATER USE: ENDING: <u>418881000</u> GAL BEGINNING: <u>418593000</u> GAL TOTAL USED: <u>288000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>89.6</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>530.9</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1451.0</u> KLB FEEDWATER USED: <u>1494.0</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>43</u> KLB BLOWDOWN: <u>2.9</u> %</p> <p>GRATE RUN TIME: ENDING: <u>73442.7</u> HRS BEGINNING: <u>73418.7</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS</p> <p>AVG. STEAM FLOW: <u>60.5</u> KLB/HR</p> <p>APPROX REF PROC: <u>226.0</u> TONS</p> <p>REFUSE PROCESSED: <u>241.8</u> TONS</p> <p>GROSS REFUSE REC: <u>436.51</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>436.51</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>1,848.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>267.45</u></p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>93.9</u> % LB STEAM/GROSS KW <u>9.8</u> LB LIME/TON PR.: <u>83.4</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>8480.0</u> WH TOT BEGINNING: <u>8470.0</u> WH TOT TOTAL: <u>288.0</u> MWH</p> <p>UTILITY OUT: ENDING: <u>7454870</u> JEM TOT BEGINNING: <u>7221610</u> JEM TOT TOTAL: <u>233.3</u> MWH</p> <p>UTILITY IN: ENDING: <u>2722250</u> JEM TOT BEGINNING: <u>2722250</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>54.7</u> MWH KWH/TON: <u>124.6</u></p> <p>MEDICAL WASTE : PROCESSED: <u>13.37</u> TONS % OF REFUSE PROC: <u>3.04</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>655.5</u> TOT STM TO T/G: <u>2,821.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>180520</u> CU FT ENDING: <u>180528</u> CU FT TOTAL USED: <u>8</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>9.1</u> FT/IN OUT BEGINNING: <u>12.8</u> FT/IN OUT RECEIVED: <u>24.12</u> TONS</p> <p>EOM OUT: <u>9.08</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>10</u> FT. OUT <u>70</u> IN OUT BEGINNING: <u>11</u> FT. OUT <u>20</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>15.83</u></p>
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EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 29, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1429.0</u> KLB FEEDWATER USED: <u>1482.0</u> KLB	STEAM PRODUCED: <u>1458.0</u> KLB FEEDWATER USED: <u>1531.0</u> KLB	GENERATOR OUT: ENDING: <u>8490.0</u> WH TOT BEGINNING: <u>8480.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>180528</u> CU FT ENDING: <u>180528</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>53</u> KLB BLOWDOWN: <u>3.6</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>73</u> KLB BLOWDOWN: <u>4.8</u> %	UTILITY OUT: ENDING: <u>7693750</u> JEM TOT BEGINNING: <u>7454870</u> JEM TOT TOTAL: <u>238.9</u> MWH	PEBBLE LIME : ENDING: <u>9.8</u> FT/IN OUT BEGINNING: <u>9.1</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>74489.1</u> HRS BEGINNING: <u>74465.1</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>73466.8</u> HRS BEGINNING: <u>73442.7</u> HRS TOTAL: <u>24.1</u> HRS	UTILITY IN: ENDING: <u>2722250</u> JEM TOT BEGINNING: <u>2722250</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>9.67</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	AVG. STEAM FLOW: <u>59.5</u> KLB/HR	AVG. STEAM FLOW: <u>60.8</u> KLB/HR
APPROX REF PROC: <u>202.8</u> TONS	APPROX REF PROC: <u>222.8</u> TONS	REFUSE PROCESSED: <u>238.2</u> TONS	REFUSE PROCESSED: <u>243.0</u> TONS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>49.1</u> MWH KWH/TON: <u>112.5</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2887.0</u> KLB TOTAL REFUSE PR. <u>436.5</u> TONS	GROSS REFUSE REC: <u>601.00</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS TOTAL REFUSE REC: <u>601.00</u> TONS		CARBON INVENTORY: ENDING: <u>22</u> FT. OUT <u>63</u> IN OUT BEGINNING: <u>10</u> FT. OUT <u>70</u> IN OUT RECEIVED: <u>20.17</u> TONS
WELL WATER USE: ENDING: <u>419189000</u> GAL BEGINNING: <u>418881000</u> GAL TOTAL USED: <u>308000</u> GAL	EST PIT INVENTORY: <u>1,968.0</u> TONS ASH HAULED: <u>0.00</u> TONS	MEDICAL WASTE : PROCESSED: <u>10.90</u> TONS % OF REFUSE PROC: <u>2.50</u> %	EOM OUT: <u>27.25</u>
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>92.5</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>547.3</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>94.3</u> % LB STEAM/GROSS KW <u>10.0</u> LB LIME/TON PR.: <u>5.0</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>659.8</u> TOT STM TO T/G: <u>2,884.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE APRIL 30, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1324.0</u> KLB	STEAM PRODUCED: <u>1348.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1370.0</u> KLB	FEEDWATER USED: <u>1423.0</u> KLB	ENDING: <u>8500.0</u> WH TOT	BEGINNING: <u>180528</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8490.0</u> WH TOT	ENDING: <u>180560</u> CU FT
BLOWDOWN: <u>46</u> KLB	BLOWDOWN: <u>75</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>32</u> CU FT
BLOWDOWN: <u>3.4</u> %	BLOWDOWN: <u>5.3</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>7915050</u> JEM TOT	ENDING: <u>10.2</u> FT/IN OUT
ENDING: <u>74513.1</u> HRS	ENDING: <u>73490.8</u> HRS	BEGINNING: <u>7693750</u> JEM TOT	BEGINNING: <u>9.8</u> FT/IN OUT
BEGINNING: <u>74489.1</u> HRS	BEGINNING: <u>73466.8</u> HRS	TOTAL: <u>221.3</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>10.17</u>
AVG. STEAM FLOW: <u>55.2</u> KLB/HR	AVG. STEAM FLOW: <u>56.2</u> KLB/HR	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>229.0</u> TONS	APPROX REF PROC: <u>223.0</u> TONS	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS <i>552</i>
REFUSE PROCESSED: <u>220.7</u> TONS	REFUSE PROCESSED: <u>224.7</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS <i>552</i>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS <i>1104</i>
TOTAL STEAM FLOW: <u>2672.0</u> KLB	GROSS REFUSE REC: <u>696.29</u> TONS	IN PLANT USE: <u>66.7</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>452.7</u> TONS	NON PROCESSED: <u>0.00</u> TONS <i>4.15</i>	KWH/TON: <u>147.3</u>	ENDING: <u>21</u> FT. OUT <u>88</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>41.16</u> TONS		BEGINNING: <u>22</u> FT. OUT <u>63</u> IN OUT
ENDING: <u>419469000</u> GAL	TOTAL REFUSE REC: <u>655.13</u> TONS <i>650.98</i>	MEDICAL WASTE :	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>419189000</u> GAL	EST PIT INVENTORY: <u>1,633.0</u> TONS	PROCESSED: <u>7.40</u> TONS	EOM OUT: <u>28.33</u>
TOTAL USED: <u>280000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.63</u> %	
	<i>101.15</i>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.7</u> %	UNIT 2 % MCR: <u>87.2</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.3</u>	GROSS KW/TON PR. <u>636.1</u>	
NET KWH/TON PR. <u>488.8</u>	LB LIME/TON PR.: <u>2.8</u>	TOT STM TO T/G: <u>2,682.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE MAY 1, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1346.0</u> KLB FEEDWATER USED: <u>1391.0</u> KLB	STEAM PRODUCED: <u>1294.0</u> KLB FEEDWATER USED: <u>1369.0</u> KLB	GENERATOR OUT: ENDING: <u>8509.0</u> WH TOT BEGINNING: <u>8500.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>180560</u> CU FT ENDING: <u>180609</u> CU FT TOTAL USED: <u>49</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>45</u> KLB BLOWDOWN: <u>3.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>75</u> KLB BLOWDOWN: <u>5.5</u> %	UTILITY OUT: ENDING: <u>8133750</u> JEM TOT BEGINNING: <u>7915050</u> JEM TOT TOTAL: <u>218.7</u> MWH	PEBBLE LIME : ENDING: <u>10.8</u> FT/IN OUT BEGINNING: <u>10.2</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>74533.1</u> HRS BEGINNING: <u>74513.1</u> HRS TOTAL: <u>20.0</u> HRS	GRATE RUN TIME: ENDING: <u>73514.8</u> HRS BEGINNING: <u>73490.8</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2722250</u> JEM TOT BEGINNING: <u>2722250</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>10.67</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>56.1</u> KLB/HR	AVG. STEAM FLOW: <u>53.9</u> KLB/HR	IN PLANT USE: <u>40.5</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>254.4</u> TONS	APPROX REF PROC: <u>247.5</u> TONS	KWH/TON: <u>89.6</u>	CARBON INVENTORY: ENDING: <u>21</u> FT. OUT <u>83</u> IN OUT BEGINNING: <u>21</u> FT. OUT <u>88</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>224.3</u> TONS	REFUSE PROCESSED: <u>215.7</u> TONS		EOM OUT: <u>27.92</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2640.0</u> KLB TOTAL REFUSE PR. <u>452.2</u> TONS <u>514.12</u>	GROSS REFUSE REC: <u>249.07</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>249.07</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>12.22</u> TONS % OF REFUSE PROC: <u>2.70</u> %	
WELL WATER USE: ENDING: <u>419757000</u> GAL BEGINNING: <u>419469000</u> GAL TOTAL USED: <u>288000</u> GAL	EST PIT INVENTORY: <u>1,860.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>105.77</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>87.1</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>483.6</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>83.7</u> % LB STEAM/GROSS KW <u>10.2</u> LB LIME/TON PR.: <u>4.2</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>573.2</u> TOT STM TO T/G: <u>2,658.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 2, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1335.0</u> KLB FEEDWATER USED: <u>1381.0</u> KLB	STEAM PRODUCED: <u>1317.0</u> KLB FEEDWATER USED: <u>1386.0</u> KLB	GENERATOR OUT: ENDING: <u>8518.0</u> WH TOT BEGINNING: <u>8509.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>180560</u> CU FT ENDING: <u>180689</u> CU FT TOTAL USED: <u>129</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>46</u> KLB BLOWDOWN: <u>3.3</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>69</u> KLB BLOWDOWN: <u>5.0</u> %	UTILITY OUT: ENDING: <u>8364300</u> JEM TOT BEGINNING: <u>8133750</u> JEM TOT TOTAL: <u>220.6</u> MWH	PEBBLE LIME : ENDING: <u>11.2</u> FT/IN OUT BEGINNING: <u>10.8</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>74542.3</u> HRS BEGINNING: <u>74533.1</u> HRS TOTAL: <u>9.2</u> HRS	GRATE RUN TIME: ENDING: <u>73538.8</u> HRS BEGINNING: <u>73514.8</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2722250</u> JEM TOT BEGINNING: <u>2722250</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>11.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>55.6</u> KLB/HR	AVG. STEAM FLOW: <u>54.9</u> KLB/HR	IN PLANT USE: <u>38.6</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>267.0</u> TONS	APPROX REF PROC: <u>263.0</u> TONS	KWH/TON: <u>87.1</u>	CARBON INVENTORY: ENDING: <u>21</u> FT. OUT <u>66</u> IN OUT BEGINNING: <u>21</u> FT. OUT <u>83</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>222.5</u> TONS	REFUSE PROCESSED: <u>219.5</u> TONS		EOM OUT: <u>28.50</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2652.0</u> KLB TOTAL REFUSE PR. <u>443.7</u> TONS <u>531.7</u>	GROSS REFUSE REC: <u>0.00</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>0.00</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>1.73</u> TONS % OF REFUSE PROC: <u>0.39</u> %	
WELL WATER USE: ENDING: <u>420043000</u> GAL BEGINNING: <u>419757000</u> GAL TOTAL USED: <u>286000</u> GAL	EST PIT INVENTORY: <u>1,358.0</u> TONS ✓ ASH HAULED: <u>0.00</u> TONS ✓		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>86.4</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>497.0</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>85.2</u> % LB STEAM/GROSS KW <u>10.2</u> LB LIME/TON PR.: <u>2.8</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>584.1</u> TOT STM TO T/G: <u>2,640.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 3 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1414.6</u> KLB FEEDWATER USED: <u>1462.5</u> KLB	STEAM PRODUCED: <u>1409.2</u> KLB FEEDWATER USED: <u>1450.8</u> KLB	GENERATOR OUT: ENDING: <u>8528.0</u> WH TOT BEGINNING: <u>8518.0</u> WH TOT TOTAL: <u>286.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>180689</u> CU FT ENDING: <u>180795</u> CU FT TOTAL USED: <u>106</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>48</u> KLB BLOWDOWN : <u>3.3</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>42</u> KLB BLOWDOWN : <u>2.9</u> %	UTILITY OUT: ENDING: <u>8589570</u> JEM TOT BEGINNING: <u>8354300</u> JEM TOT TOTAL: <u>235.3</u> MWH	PEBBLE LIME : ENDING: <u>12.0</u> FT/IN OUT BEGINNING: <u>11.2</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>74566.3</u> HRS BEGINNING: <u>74542.3</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>73562.8</u> HRS BEGINNING: <u>73538.8</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2722250</u> JEM TOT BEGINNING: <u>2722250</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>12.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>58.9</u> KLB/HR	AVG. STEAM FLOW: <u>58.7</u> KLB/HR	IN PLANT USE: <u>52.7</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>220.8</u> TONS	APPROX REF PROC: <u>190.3</u> TONS	KWH/TON: <u>124.9</u>	CARBON INVENTORY: ENDING: <u>21</u> FT. OUT <u>41</u> IN OUT BEGINNING: <u>21</u> FT. OUT <u>68</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>235.8</u> TONS	REFUSE PROCESSED: <u>234.9</u> TONS		EOM OUT: <u>24.42</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2823.8</u> KLB TOTAL REFUSE PR. <u>422.3</u> TONS <u>481.95</u>	GROSS REFUSE REC: <u>754.74</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>754.74</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>11.25</u> TONS % OF REFUSE PROC: <u>2.86</u> %	
WELL WATER USE: ENDING: <u>420346000</u> GAL BEGINNING: <u>420043000</u> GAL TOTAL USED: <u>303000</u> GAL	EST PIT INVENTORY: <u>1,692.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>149.17</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>91.5</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>557.1</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>91.2</u> % LB STEAM/GROSS KW <u>9.8</u> LB LIME/TON PR.: <u>5.9</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>681.9</u> TOT STM TO T/G: <u>2,580.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 4 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1420.2</u> KLB	STEAM PRODUCED: <u>1436.1</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1469.3</u> KLB	FEEDWATER USED: <u>1479.3</u> KLB	ENDING: <u>8538.0</u> WH TOT	BEGINNING: <u>180795</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8528.0</u> WH TOT	ENDING: <u>180803</u> CU FT
BLOWDOWN: <u>49</u> KLB	BLOWDOWN: <u>43</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>8</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>2.9</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>8829480</u> JEM TOT	ENDING: <u>13.2</u> FT/IN OUT
ENDING: <u>74590.3</u> HRS	ENDING: <u>73586.8</u> HRS	BEGINNING: <u>8589570</u> JEM TOT	BEGINNING: <u>12.0</u> FT/IN OUT
BEGINNING: <u>74566.3</u> HRS	BEGINNING: <u>73562.8</u> HRS	TOTAL: <u>239.9</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>13.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.2</u> KLB/HR	AVG. STEAM FLOW: <u>59.8</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>161.2</u> TONS	APPROX REF PROC: <u>169.6</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>236.7</u> TONS	REFUSE PROCESSED: <u>239.4</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>48.1</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>141.5</u>	ENDING: <u>21</u> FT. OUT <u>10</u> IN OUT
TOTAL STEAM FLOW: <u>2856.3</u> KLB	GROSS REFUSE REC: <u>719.66</u> TONS		BEGINNING: <u>21</u> FT. OUT <u>41</u> IN OUT
TOTAL REFUSE PR. <u>339.9</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
<u>485.17</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>21.83</u>
WELL WATER USE:	TOTAL REFUSE REC: <u>719.66</u> TONS <u>716.16</u>	MEDICAL WASTE:	
ENDING: <u>420652000</u> GAL	EST PIT INVENTORY: <u>2,070.0</u> TONS	PROCESSED: <u>9.07</u> TONS	
BEGINNING: <u>420346000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.67</u> %	
TOTAL USED: <u>306000</u> GAL	<u>52.38</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>91.9</u> %	UNIT 2 % MCR: <u>92.9</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.9</u>	GROSS KW/TON PR. <u>847.4</u>	
NET KWH/TON PR. <u>705.9</u>	LB LIME/TON PR.: <u>11.1</u>	TOT STM TO T/G: <u>2,856.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 5, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1426.0</u> KLB	STEAM PRODUCED: <u>1429.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1475.0</u> KLB	FEEDWATER USED: <u>1488.0</u> KLB	ENDING: <u>8548.0</u> WH TOT	BEGINNING: <u>180803</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8538.0</u> WH TOT	ENDING: <u>180803</u> CU FT
BLOWDOWN: <u>49</u> KLB	BLOWDOWN: <u>59</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>4.0</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>9068880</u> JEM TOT	ENDING: <u>9.0</u> FT/IN OUT
ENDING: <u>74614.3</u> HRS	ENDING: <u>73610.8</u> HRS	BEGINNING: <u>8829480</u> JEM TOT	BEGINNING: <u>13.2</u> FT/IN OUT
BEGINNING: <u>74590.3</u> HRS	BEGINNING: <u>73588.8</u> HRS	TOTAL: <u>239.4</u> MWH	RECEIVED: <u>24.57</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>9.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2722250</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.4</u> KLB/HR	AVG. STEAM FLOW: <u>59.5</u> KLB/HR	BEGINNING: <u>2722250</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>179.7</u> TONS	APPROX REF PROC: <u>167.6</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>237.7</u> TONS	REFUSE PROCESSED: <u>238.2</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>48.6</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>137.9</u>	ENDING: <u>21</u> FT. OUT <u>0</u> IN OUT
TOTAL STEAM FLOW: <u>2855.0</u> KLB	GROSS REFUSE REC: <u>579.23</u> TONS		BEGINNING: <u>21</u> FT. OUT <u>10</u> IN OUT
TOTAL REFUSE PR. <u>352.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
<i>48609</i>	FERROUS HAULED: <u>0.00</u> TONS		EOM OUT: <u>21.00</u>
WELL WATER USE:	TOTAL REFUSE REC: <u>579.23</u> TONS <i>578.03</i>	MEDICAL WASTE :	
ENDING: <u>420968000</u> GAL	EST PIT INVENTORY: <u>1,926.0</u> TONS	PROCESSED: <u>5.19</u> TONS	
BEGINNING: <u>420652000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.47</u> %	
TOTAL USED: <u>304000</u> GAL	<i>222.88</i>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>92.3</u> %	UNIT 2 % MCR: <u>92.5</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.9</u>	GROSS KW/TON PR. <u>817.1</u>	
NET KWH/TON PR. <u>679.2</u>	LB LIME/TON PR.: <u>102.0</u>	TOT STM TO T/G: <u>2,871.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 6, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1414.0</u> KLB FEEDWATER USED: <u>1462.0</u> KLB	STEAM PRODUCED: <u>1419.0</u> KLB FEEDWATER USED: <u>1482.0</u> KLB	GENERATOR OUT: ENDING: <u>8557.0</u> WH TOT BEGINNING: <u>8548.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>180803</u> CU FT ENDING: <u>180804</u> CU FT TOTAL USED: <u>1</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>48</u> KLB BLOWDOWN: <u>3.3</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>63</u> KLB BLOWDOWN: <u>4.3</u> %	UTILITY OUT: ENDING: <u>9304090</u> JEM TOT BEGINNING: <u>9068880</u> JEM TOT TOTAL: <u>235.2</u> MWH	PEBBLE LIME : ENDING: <u>9.6</u> FT/IN OUT BEGINNING: <u>9.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>74638.3</u> HRS BEGINNING: <u>74614.3</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>73634.8</u> HRS BEGINNING: <u>73610.8</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2722250</u> JEM TOT BEGINNING: <u>2722250</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>9.50</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>58.9</u> KLB/HR APPROX REF PROC: <u>148.0</u> TONS	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>59.1</u> KLB/HR APPROX REF PROC: <u>153.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>24.0</u> MWH KWH/TON: <u>78.5</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
REFUSE PROCESSED: <u>235.7</u> TONS NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB	REFUSE PROCESSED: <u>238.5</u> TONS TOTAL STEAM FLOW: <u>2833.0</u> KLB TOTAL REFUSE PR. <u>305.6</u> TONS <u>476.77</u>		CARBON INVENTORY: ENDING: <u>20</u> FT. OUT <u>59</u> IN OUT BEGINNING: <u>21</u> FT. OUT <u>0</u> IN OUT RECEIVED: <u>0.00</u> TONS
WELL WATER USE: ENDING: <u>421263000</u> GAL BEGINNING: <u>420956000</u> GAL TOTAL USED: <u>307000</u> GAL	GROSS REFUSE REC: <u>513.00</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS TOTAL REFUSE REC: <u>513.00</u> TONS ✓ EST PIT INVENTORY: <u>1,867.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>183.93</u>	MEDICAL WASTE : PROCESSED: <u>4.57</u> TONS % OF REFUSE PROC: <u>1.50</u> %	EOM OUT: <u>24.92</u>
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>91.5</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>769.7</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>91.8</u> % LB STEAM/GROSS KW <u>10.9</u> LB LIME/TON PR.: <u>6.2</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>848.3</u> TOT STM TO T/G: <u>2,847.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
 DAILY PRODUCTION REPORT
 DATE MAY 7, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1432.0</u> KLB FEEDWATER USED: <u>1479.0</u> KLB	STEAM PRODUCED: <u>1466.0</u> KLB FEEDWATER USED: <u>1509.0</u> KLB	GENERATOR OUT: ENDING: <u>8566.0</u> WH TOT BEGINNING: <u>8557.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>180804</u> CU FT ENDING: <u>180807</u> CU FT TOTAL USED: <u>3</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>47</u> KLB BLOWDOWN: <u>3.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>43</u> KLB BLOWDOWN: <u>2.8</u> %	UTILITY OUT: ENDING: <u>9514700</u> JEM TOT BEGINNING: <u>9304090</u> JEM TOT TOTAL: <u>210.6</u> MWH	PEBBLE LIME : ENDING: <u>10.3</u> FT/IN OUT BEGINNING: <u>9.6</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>74662.3</u> HRS BEGINNING: <u>74638.3</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>73658.8</u> HRS BEGINNING: <u>73634.8</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2727800</u> JEM TOT BEGINNING: <u>2722250</u> JEM TOT TOTAL: <u>5.6</u> MWH	EOM OUT: <u>10.25</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>59.7</u> KLB/HR APPROX REF PROC: <u>212.0</u> TONS	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>61.1</u> KLB/HR APPROX REF PROC: <u>204.0</u> TONS	GENERATOR RUN TIME: <u>21.3</u> HRS IN PLANT USE: <u>54.1</u> MWH KWH/TON: <u>126.8</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
REFUSE PROCESSED: <u>238.7</u> TONS	REFUSE PROCESSED: <u>244.3</u> TONS		CARBON INVENTORY: ENDING: <u>20</u> FT. OUT <u>17</u> IN OUT BEGINNING: <u>20</u> FT. OUT <u>59</u> IN OUT RECEIVED: <u>0.00</u> TONS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			EOM OUT: <u>21.42</u>
TOTAL STEAM FLOW: <u>2898.0</u> KLB TOTAL REFUSE PR. <u>427.1</u> TONS <u>494.12</u>	GROSS REFUSE REC: <u>627.44</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>627.44</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>11.12</u> TONS % OF REFUSE PROC: <u>2.60</u> %	
WELL WATER USE: ENDING: <u>421554000</u> GAL BEGINNING: <u>421263000</u> GAL TOTAL USED: <u>291000</u> GAL	EST PIT INVENTORY: <u>2,130.0</u> TONS ✓ ASH HAULED: <u>0.00</u> TONS ✓		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>92.7</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>493.1</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>94.8</u> % LB STEAM/GROSS KW <u>11.2</u> LB LIME/TON PR.: <u>5.1</u>	TG AVAILABILITY: <u>88.8</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>606.9</u> TOT STM TO T/G: <u>2,874.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

- T/G off line for 2.7 hours due to lightning.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 8 1999

<p>BOILER NO. 1</p> <p>STEAM PRODUCED: <u>1469.5</u> KLB FEEDWATER USED: <u>1520.5</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>51</u> KLB BLOWDOWN : <u>3.4</u> %</p> <p>GRATE RUN TIME: ENDING: <u>74686.3</u> HRS BEGINNING: <u>74662.3</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>61.2</u> KLB/HR APPROX REF PROC: <u>157.3</u> TONS REFUSE PROCESSED: <u>244.9</u> TONS</p> <p>TOTAL STEAM FLOW: <u>3000.4</u> KLB TOTAL REFUSE PR. <u>348.3</u> TONS <i>506.25</i></p> <p>WELL WATER USE: ENDING: <u>421832000</u> GAL BEGINNING: <u>421554000</u> GAL TOTAL USED: <u>278000</u> GAL</p> <p>UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>95.1</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>721.4</u></p>	<p>BOILER NO. 2</p> <p>STEAM PRODUCED: <u>1530.9</u> KLB FEEDWATER USED: <u>1582.2</u> KLB</p> <p>BOILER BLOWDOWN: BLOWDOWN: <u>51</u> KLB BLOWDOWN : <u>3.2</u> %</p> <p>GRATE RUN TIME: ENDING: <u>73682.8</u> HRS BEGINNING: <u>73658.8</u> HRS TOTAL: <u>24.0</u> HRS</p> <p>BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>63.8</u> KLB/HR APPROX REF PROC: <u>184.9</u> TONS REFUSE PROCESSED: <u>255.2</u> TONS</p> <p>GROSS REFUSE REC: <u>260.47</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>260.47</u> TONS ✓</p> <p>EST PIT INVENTORY: <u>1,867.0</u> TONS ASH HAULED: <u>0.00</u> TONS <i>98.05</i></p> <p>UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>99.0</u> % LB STEAM/GROSS KW <u>10.4</u> LB LIME/TON PR.: <u>6.3</u></p>	<p>ELECTRICITY</p> <p>GENERATOR OUT: ENDING: <u>8576.0</u> WH TOT BEGINNING: <u>8566.0</u> WH TOT TOTAL: <u>288.0</u> MWH</p> <p>UTILITY OUT: ENDING: <u>9765980</u> JEM TOT BEGINNING: <u>9514700</u> JEM TOT TOTAL: <u>251.3</u> MWH</p> <p>UTILITY IN: ENDING: <u>2727800</u> JEM TOT BEGINNING: <u>2727800</u> JEM TOT TOTAL: <u>0.0</u> MWH</p> <p>GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>36.7</u> MWH KWH/TON: <u>105.4</u></p> <p>MEDICAL WASTE : PROCESSED: <u>6.15</u> TONS % OF REFUSE PROC: <u>1.77</u> %</p> <p>TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>826.8</u> TOT STM TO T/G: <u>3,031.0</u></p>	<p>INVENTORY</p> <p>NATURAL GAS USAGE: BEGINNING: <u>180807</u> CU FT ENDING: <u>180807</u> CU FT TOTAL USED: <u>0</u> CU FT</p> <p>PEBBLE LIME : ENDING: <u>11.0</u> FT/IN OUT BEGINNING: <u>10.3</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>11.00</u></p> <p>CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS</p> <p>DAILY TOTAL: <u>538</u> LBS</p> <p>CARBON INVENTORY: ENDING: <u>19</u> FT. OUT <u>95</u> IN OUT BEGINNING: <u>20</u> FT. OUT <u>17</u> IN OUT RECEIVED: <u>0.00</u> TONS</p> <p>EOM OUT: <u>26.92</u></p>
<p>NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB</p>			

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 9 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1330.9</u> KLB	STEAM PRODUCED: <u>1397.7</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1375.3</u> KLB	FEEDWATER USED: <u>1474.2</u> KLB	ENDING: <u>8586.0</u> WH TOT	BEGINNING: <u>180807</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8576.0</u> WH TOT	ENDING: <u>180828</u> CU FT
BLOWDOWN: <u>44</u> KLB	BLOWDOWN: <u>77</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>21</u> CU FT
BLOWDOWN: <u>3.2</u> %	BLOWDOWN: <u>5.2</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>9990240</u> JEM TOT	ENDING: <u>11.4</u> FT/IN OUT
ENDING: <u>74709.3</u> HRS	ENDING: <u>73706.8</u> HRS	BEGINNING: <u>9765980</u> JEM TOT	BEGINNING: <u>11.0</u> FT/IN OUT
BEGINNING: <u>74685.3</u> HRS	BEGINNING: <u>73682.8</u> HRS	TOTAL: <u>224.3</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>11.33</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.5</u> KLB/HR	AVG. STEAM FLOW: <u>58.2</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>144.1</u> TONS	APPROX REF PROC: <u>142.3</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>221.8</u> TONS	REFUSE PROCESSED: <u>233.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>63.7</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>222.5</u>	ENDING: <u>19</u> FT. OUT <u>63</u> IN OUT
TOTAL STEAM FLOW: <u>2728.6</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS		BEGINNING: <u>19</u> FT. OUT <u>95</u> IN OUT
TOTAL REFUSE PR. <u>286.4</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
<u>454.8</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>24.25</u>
WELL WATER USE:	TOTAL REFUSE REC: <u>0.00</u> TONS ✓	MEDICAL WASTE:	
ENDING: <u>422098000</u> GAL	EST PIT INVENTORY: <u>1,342.0</u> TONS ✓	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>421832000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>266000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>86.1</u> %	UNIT 2 % MCR: <u>90.4</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.5</u>	GROSS KW/TON PR. <u>1005.5</u>	
NET KWH/TON PR. <u>782.9</u>	LB LIME/TON PR.: <u>4.4</u>	TOT STM TO T/G: <u>2,758.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 10 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1300.1</u> KLB	STEAM PRODUCED: <u>1365.6</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1341.9</u> KLB	FEEDWATER USED: <u>1426.7</u> KLB	ENDING: <u>8596.0</u> WH TOT	BEGINNING: <u>180828</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8586.0</u> WH TOT	ENDING: <u>180834</u> CU FT
BLOWDOWN: <u>42</u> KLB	BLOWDOWN: <u>61</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>6</u> CU FT
BLOWDOWN: <u>3.1</u> %	BLOWDOWN: <u>4.3</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>10209270</u> JEM TOT	ENDING: <u>12.4</u> FT/IN OUT
ENDING: <u>74733.3</u> HRS	ENDING: <u>73730.8</u> HRS	BEGINNING: <u>9990240</u> JEM TOT	BEGINNING: <u>11.4</u> FT/IN OUT
BEGINNING: <u>74709.3</u> HRS	BEGINNING: <u>73706.8</u> HRS	TOTAL: <u>219.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>12.33</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>54.2</u> KLB/HR	AVG. STEAM FLOW: <u>56.9</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>232.0</u> TONS	APPROX REF PROC: <u>227.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>216.7</u> TONS	REFUSE PROCESSED: <u>227.6</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>69.0</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>153.8</u>	ENDING: <u>19</u> FT. OUT <u>21</u> IN OUT
TOTAL STEAM FLOW: <u>2665.7</u> KLB	GROSS REFUSE REC: <u>673.08</u> TONS		BEGINNING: <u>19</u> FT. OUT <u>63</u> IN OUT
TOTAL REFUSE PR. <u>448.4</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>20.75</u>
	TOTAL REFUSE REC: <u>673.08</u> TONS ✓		
WELL WATER USE:	EST PIT INVENTORY: <u>1,634.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>422360000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>4.12</u> TONS	
BEGINNING: <u>422098000</u> GAL		% OF REFUSE PROC: <u>0.92</u> %	
TOTAL USED: <u>262000</u> GAL	<u>154.43</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>84.1</u> %	UNIT 2 % MCR: <u>88.4</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.3</u>	GROSS KW/TON PR. <u>642.3</u>	
NET KWH/TON PR. <u>488.5</u>	LB LIME/TON PR.: <u>7.0</u>	TOT STM TO T/G: <u>2,675.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 11 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1352.5</u> KLB FEEDWATER USED: <u>1397.1</u> KLB	STEAM PRODUCED: <u>1450.5</u> KLB FEEDWATER USED: <u>1523.7</u> KLB	GENERATOR OUT: ENDING: <u>8605.0</u> WH TOT BEGINNING: <u>8596.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>180834</u> CU FT ENDING: <u>180835</u> CU FT TOTAL USED: <u>1</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>45</u> KLB BLOWDOWN: <u>3.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>73</u> KLB BLOWDOWN: <u>4.8</u> %	UTILITY OUT: ENDING: <u>442030</u> JEM TOT BEGINNING: <u>209270</u> JEM TOT TOTAL: <u>232.8</u> MWH	PEBBLE LIME : ENDING: <u>9.0</u> FT/IN OUT BEGINNING: <u>12.4</u> FT/IN OUT RECEIVED: <u>25.72</u> TONS
GRATE RUN TIME: ENDING: <u>74757.3</u> HRS BEGINNING: <u>74733.3</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>73754.8</u> HRS BEGINNING: <u>73730.8</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2727800</u> JEM TOT BEGINNING: <u>2727800</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>9.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>56.4</u> KLB/HR	AVG. STEAM FLOW: <u>60.4</u> KLB/HR	IN PLANT USE: <u>26.4</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>230.1</u> TONS	APPROX REF PROC: <u>231.0</u> TONS	KWH/TON: <u>56.6</u>	CARBON INVENTORY: ENDING: <u>18</u> FT. OUT <u>46</u> IN OUT BEGINNING: <u>19</u> FT. OUT <u>21</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>225.4</u> TONS	REFUSE PROCESSED: <u>241.8</u> TONS		EOM OUT: <u>21.83</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2803.0</u> KLB TOTAL REFUSE PR. <u>466.7</u> TONS	GROSS REFUSE REC: <u>629.01</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>629.01</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>5.63</u> TONS % OF REFUSE PROC: <u>1.21</u> %	
WELL WATER USE: ENDING: <u>422630000</u> GAL BEGINNING: <u>422360000</u> GAL TOTAL USED: <u>270000</u> GAL	EST PIT INVENTORY: <u>1,867.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>255.89</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>87.5</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>498.7</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>93.8</u> % LB STEAM/GROSS KW <u>10.8</u> LB LIME/TON PR.: <u>87.3</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>555.4</u> TOT STM TO T/G: <u>2,826.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 12 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1424.6</u> KLB FEEDWATER USED: <u>1471.9</u> KLB	STEAM PRODUCED: <u>1450.6</u> KLB FEEDWATER USED: <u>1532.5</u> KLB	GENERATOR OUT: ENDING: <u>8615.0</u> WH TOT BEGINNING: <u>8605.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>180835</u> CU FT ENDING: <u>180836</u> CU FT TOTAL USED: <u>1</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>47</u> KLB BLOWDOWN : <u>3.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>82</u> KLB BLOWDOWN : <u>5.3</u> %	UTILITY OUT: ENDING: <u>684560</u> JEM TOT BEGINNING: <u>442030</u> JEM TOT TOTAL: <u>242.5</u> MWH	PEBBLE LIME : ENDING: <u>10.0</u> FT/IN OUT BEGINNING: <u>9.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>74781.3</u> HRS BEGINNING: <u>74757.3</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>73778.8</u> HRS BEGINNING: <u>73754.8</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2727800</u> JEM TOT BEGINNING: <u>2727800</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>10.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS
AVG. STEAM FLOW: <u>59.4</u> KLB/HR	AVG. STEAM FLOW: <u>60.4</u> KLB/HR	IN PLANT USE: <u>45.5</u> MWH	DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>244.0</u> TONS	APPROX REF PROC: <u>232.0</u> TONS	KWH/TON: <u>92.8</u>	CARBON INVENTORY: ENDING: <u>18</u> FT. OUT <u>78</u> IN OUT BEGINNING: <u>18</u> FT. OUT <u>48</u> IN OUT RECEIVED: <u>0.00</u> TONS
REFUSE PROCESSED: <u>237.4</u> TONS	REFUSE PROCESSED: <u>241.8</u> TONS		EOM OUT: <u>24.50</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2875.2</u> KLB TOTAL REFUSE PR. <u>490.0</u> TONS	GROSS REFUSE REC: <u>610.83</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>610.83</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>13.98</u> TONS % OF REFUSE PROC: <u>2.85</u> %	
WELL WATER USE: ENDING: <u>422807000</u> GAL BEGINNING: <u>422630000</u> GAL TOTAL USED: <u>277000</u> GAL	EST PIT INVENTORY: <u>1,284.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>97.59</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>92.2</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>495.0</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>93.9</u> % LB STEAM/GROSS KW <u>10.0</u> LB LIME/TON PR.: <u>6.4</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>587.8</u> TOT STM TO T/G: <u>2,918.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 13, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1383.1</u> KLB	STEAM PRODUCED: <u>1392.3</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1430.0</u> KLB	FEEDWATER USED: <u>1451.0</u> KLB	ENDING: <u>8625.0</u> WH TOT	BEGINNING: <u>180836</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8615.0</u> WH TOT	ENDING: <u>180836</u> CU FT
BLOWDOWN: <u>47</u> KLB	BLOWDOWN: <u>59</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>4.0</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>913150</u> JEM TOT	ENDING: <u>11.3</u> FT/IN OUT
ENDING: <u>74805.3</u> HRS	ENDING: <u>73802.6</u> HRS	BEGINNING: <u>684560</u> JEM TOT	BEGINNING: <u>10.0</u> FT/IN OUT
BEGINNING: <u>74781.3</u> HRS	BEGINNING: <u>73778.8</u> HRS	TOTAL: <u>228.6</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.8</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>11.21</u>
AVG. STEAM FLOW: <u>57.6</u> KLB/HR	AVG. STEAM FLOW: <u>58.0</u> KLB/HR	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>222.0</u> TONS	APPROX REF PROC: <u>231.0</u> TONS	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>230.5</u> TONS	REFUSE PROCESSED: <u>232.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2775.4</u> KLB	GROSS REFUSE REC: <u>425.28</u> TONS	IN PLANT USE: <u>59.4</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>460.3</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>129.1</u>	ENDING: <u>17</u> FT. OUT <u>97</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓	MEDICAL WASTE:	BEGINNING: <u>18</u> FT. OUT <u>78</u> IN OUT
ENDING: <u>423182000</u> GAL	TOTAL REFUSE REC: <u>425.28</u> TONS ✓	PROCESSED: <u>7.28</u> TONS	RECEIVED: <u>0.00</u> TONS
BEGINNING: <u>422907000</u> GAL	EST PIT INVENTORY: <u>1,575.0</u> TONS	% OF REFUSE PROC: <u>1.58</u> %	EOM OUT: <u>25.08</u>
TOTAL USED: <u>255000</u> GAL	ASH HAULED: <u>0.00</u> TONS		
	<u>137.91</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>89.5</u> %	UNIT 2 % MCR: <u>90.1</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>8.6</u>	GROSS KW/TON PR. <u>625.7</u>	
NET KWH/TON PR. <u>496.6</u>	LB LIME/TON PR.: <u>8.5</u>	TOT STM TO T/G: <u>2,784.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 14, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1260.1</u> KLB	STEAM PRODUCED: <u>1311.7</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1300.3</u> KLB	FEEDWATER USED: <u>1375.8</u> KLB	ENDING: <u>8633.0</u> WH TOT	BEGINNING: <u>180836</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8625.0</u> WH TOT	ENDING: <u>180876</u> CU FT
BLOWDOWN: <u>40</u> KLB	BLOWDOWN: <u>64</u> KLB	TOTAL: <u>230.4</u> MWH	TOTAL USED: <u>40</u> CU FT
BLOWDOWN %: <u>3.1</u> %	BLOWDOWN %: <u>4.7</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1119340</u> JEM TOT	ENDING: <u>11.7</u> FT/IN OUT
ENDING: <u>74829.3</u> HRS	ENDING: <u>73826.1</u> HRS	BEGINNING: <u>913150</u> JEM TOT	BEGINNING: <u>11.3</u> FT/IN OUT
BEGINNING: <u>74805.3</u> HRS	BEGINNING: <u>73802.6</u> HRS	TOTAL: <u>206.2</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.5</u> HRS	UTILITY IN:	EOM OUT: <u>11.55</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>52.5</u> KLB/HR	AVG. STEAM FLOW: <u>54.7</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>161.0</u> TONS	APPROX REF PROC: <u>163.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>210.0</u> TONS	REFUSE PROCESSED: <u>218.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>24.2</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2571.8</u> KLB	GROSS REFUSE REC: <u>79.71</u> TONS	KWH/TON: <u>74.7</u>	ENDING: <u>18</u> FT. OUT <u>9</u> IN OUT
TOTAL REFUSE PR. <u>324.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>17</u> FT. OUT <u>97</u> IN OUT
<u>424.6</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	TOTAL REFUSE REC: <u>79.71</u> TONS ✓	MEDICAL WASTE :	EOM OUT: <u>16.75</u>
ENDING: <u>423406000</u> GAL	EST PIT INVENTORY: <u>1,050.0</u> TONS	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>423162000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>244000</u> GAL	<u>130.26</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>81.5</u> %	UNIT 2 % MCR: <u>84.9</u> %	TG % MCR: <u>61.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>11.2</u>	GROSS KW/TON PR. <u>711.1</u>	
NET KWH/TON PR. <u>638.4</u>	LB LIME/TON PR.: <u>3.5</u>	TOT STM TO T/G: <u>2,555.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 15, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1279.6</u> KLB	STEAM PRODUCED: <u>1328.2</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1322.7</u> KLB	FEEDWATER USED: <u>1383.4</u> KLB	ENDING: <u>8643.0</u> WH TOT	BEGINNING: <u>180876</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8633.0</u> WH TOT	ENDING: <u>180885</u> CU FT
BLOWDOWN: <u>43</u> KLB	BLOWDOWN: <u>55</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>9</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>4.0</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1332190</u> JEM TOT	ENDING: <u>12.0</u> FT/IN OUT
ENDING: <u>74853.3</u> HRS	ENDING: <u>73850.1</u> HRS	BEGINNING: <u>1119340</u> JEM TOT	BEGINNING: <u>11.7</u> FT/IN OUT
BEGINNING: <u>74829.3</u> HRS	BEGINNING: <u>73826.1</u> HRS	TOTAL: <u>212.9</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>12.00</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>53.3</u> KLB/HR	AVG. STEAM FLOW: <u>55.3</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>201.0</u> TONS	APPROX REF PROC: <u>202.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>213.3</u> TONS	REFUSE PROCESSED: <u>221.4</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>75.2</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2807.7</u> KLB	GROSS REFUSE REC: <u>398.63</u> TONS	KWH/TON: <u>176.4</u>	ENDING: <u>17</u> FT. OUT <u>35</u> IN OUT
TOTAL REFUSE PR. <u>426.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>18</u> FT. OUT <u>9</u> IN OUT
	FERROUS HAULED: <u>32.63</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>366.00</u> TONS ✓		EOM OUT: <u>19.92</u>
WELL WATER USE:	EST PIT INVENTORY: <u>1,458.0</u> TONS	MEDICAL WASTE :	
ENDING: <u>423670000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>23.00</u> TONS	
BEGINNING: <u>423406000</u> GAL	<u>165.24</u>	% OF REFUSE PROC: <u>5.40</u> %	
TOTAL USED: <u>264000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>82.8</u> %	UNIT 2 % MCR: <u>85.9</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.1</u>	GROSS KW/TON PR. <u>676.1</u>	
NET KWH/TON PR. <u>499.6</u>	LB LIME/TON PR.: <u>2.2</u>	TOT STM TO T/G: <u>2,619.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 16, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1324.1</u> KLB FEEDWATER USED: <u>1368.3</u> KLB	STEAM PRODUCED: <u>1362.9</u> KLB FEEDWATER USED: <u>1428.3</u> KLB	GENERATOR OUT: ENDING: <u>8652.0</u> WH TOT BEGINNING: <u>8643.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>180885</u> CU FT ENDING: <u>180936</u> CU FT TOTAL USED: <u>51</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>44</u> KLB BLOWDOWN : <u>3.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>65</u> KLB BLOWDOWN : <u>4.6</u> %	UTILITY OUT: ENDING: <u>1554340</u> JEM TOT BEGINNING: <u>1332190</u> JEM TOT TOTAL: <u>222.2</u> MWH	PEBBLE LIME : ENDING: <u>12.7</u> FT/IN OUT BEGINNING: <u>12.0</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>74877.3</u> HRS BEGINNING: <u>74853.3</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>73873.8</u> HRS BEGINNING: <u>73850.1</u> HRS TOTAL: <u>23.7</u> HRS	UTILITY IN: ENDING: <u>2727800</u> JEM TOT BEGINNING: <u>2727800</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>12.55</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>55.2</u> KLB/HR	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>56.8</u> KLB/HR	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>37.0</u> MWH KWH/TON: <u>82.7</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>279.8</u> TONS REFUSE PROCESSED: <u>220.7</u> TONS	APPROX REF PROC: <u>271.3</u> TONS REFUSE PROCESSED: <u>227.2</u> TONS		CARBON INVENTORY: ENDING: <u>16</u> FT. OUT <u>69</u> IN OUT BEGINNING: <u>17</u> FT. OUT <u>35</u> IN OUT RECEIVED: <u>0.00</u> TONS EOM OUT: <u>21.75</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2687.0</u> KLB TOTAL REFUSE PR. <u>447.8</u> TONS	GROSS REFUSE REC: <u>0.00</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>0.00</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	
WELL WATER USE: ENDING: <u>423932000</u> GAL BEGINNING: <u>423870000</u> GAL TOTAL USED: <u>262000</u> GAL	EST PIT INVENTORY: <u>817.0</u> TONS ASH HAULED: <u>0.00</u> TONS ✓		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>85.7</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>498.1</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>88.2</u> % LB STEAM/GROSS KW <u>10.4</u> LB LIME/TON PR.: <u>4.8</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>578.8</u> TOT STM TO T/G: <u>2,717.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 17, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1321.0</u> KLB	STEAM PRODUCED: <u>1362.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1362.0</u> KLB	FEEDWATER USED: <u>1438.0</u> KLB	ENDING: <u>8661.0</u> WH TOT	BEGINNING: <u>180936</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8652.0</u> WH TOT	ENDING: <u>181177</u> CU FT
BLOWDOWN: <u>41</u> KLB	BLOWDOWN: <u>76</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>241</u> CU FT
BLOWDOWN %: <u>3.0</u> %	BLOWDOWN %: <u>5.3</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>1774700</u> JEM TOT	ENDING: <u>13.5</u> FT/IN OUT
ENDING: <u>74901.3</u> HRS	ENDING: <u>73897.8</u> HRS	BEGINNING: <u>1554340</u> JEM TOT	BEGINNING: <u>12.7</u> FT/IN OUT
BEGINNING: <u>74877.3</u> HRS	BEGINNING: <u>73873.8</u> HRS	TOTAL: <u>220.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>13.42</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>55.0</u> KLB/HR	AVG. STEAM FLOW: <u>56.8</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>238.0</u> TONS	APPROX REF PROC: <u>255.8</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>220.2</u> TONS	REFUSE PROCESSED: <u>227.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>38.8</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2683.0</u> KLB	GROSS REFUSE REC: <u>713.68</u> TONS	KWH/TON: <u>85.9</u>	ENDING: <u>16</u> FT. OUT <u>52</u> IN OUT
TOTAL REFUSE PR. <u>452.4</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>16</u> FT. OUT <u>69</u> IN OUT
<u>497</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	TOTAL REFUSE REC: <u>713.68</u> TONS ✓	MEDICAL WASTE :	EOM OUT: <u>20.33</u>
ENDING: <u>424205000</u> GAL	EST PIT INVENTORY: <u>1,225.0</u> TONS	PROCESSED: <u>5.21</u> TONS	
BEGINNING: <u>423932000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>1.15</u> %	
TOTAL USED: <u>273000</u> GAL	<u>37.78</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>85.5</u> %	UNIT 2 % MCR: <u>88.1</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.4</u>	GROSS KW/TON PR. <u>573.0</u>	
NET KWH/TON PR. <u>487.1</u>	LB LIME/TON PR.: <u>5.6</u>	TOT STM TO T/G: <u>2,630.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 18, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1397.0</u> KLB FEEDWATER USED: <u>1443.5</u> KLB	STEAM PRODUCED: <u>1407.5</u> KLB FEEDWATER USED: <u>1473.5</u> KLB	GENERATOR OUT: ENDING: <u>8671.0</u> WH TOT BEGINNING: <u>8661.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>181177</u> CU FT ENDING: <u>181184</u> CU FT TOTAL USED: <u>7</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>47</u> KLB BLOWDOWN: <u>3.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>66</u> KLB BLOWDOWN: <u>4.5</u> %	UTILITY OUT: ENDING: <u>2005760</u> JEM TOT BEGINNING: <u>1774700</u> JEM TOT TOTAL: <u>231.1</u> MWH	PEBBLE LIME : ENDING: <u>10.5</u> FT/IN OUT BEGINNING: <u>13.5</u> FT/IN OUT RECEIVED: <u>24.27</u> TONS
GRATE RUN TIME: ENDING: <u>74925.3</u> HRS BEGINNING: <u>74901.3</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>73921.8</u> HRS BEGINNING: <u>73897.8</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2727800</u> JEM TOT BEGINNING: <u>2727800</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>10.42</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>58.2</u> KLB/HR APPROX REF PROC: <u>206.3</u> TONS	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>58.6</u> KLB/HR APPROX REF PROC: <u>214.6</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>56.9</u> MWH KWH/TON: <u>132.4</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
REFUSE PROCESSED: <u>232.8</u> TONS	REFUSE PROCESSED: <u>234.6</u> TONS		CARBON INVENTORY: ENDING: <u>16</u> FT. OUT <u>30</u> IN OUT BEGINNING: <u>16</u> FT. OUT <u>52</u> IN OUT RECEIVED: <u>0.00</u> TONS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			EOM OUT: <u>18.50</u>
TOTAL STEAM FLOW: <u>2804.5</u> KLB TOTAL REFUSE PR. <u>430.1</u> TONS <i>476.62</i>	GROSS REFUSE REC: <u>714.53</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>714.53</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>9.22</u> TONS % OF REFUSE PROC: <u>2.74</u> %	
WELL WATER USE: ENDING: <u>424468000</u> GAL BEGINNING: <u>424205000</u> GAL TOTAL USED: <u>263000</u> GAL	EST PIT INVENTORY: <u>1,576.0</u> TONS ASH HAULED: <u>0.00</u> TONS <i>184.26</i>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>90.4</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>537.2</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>91.1</u> % LB STEAM/GROSS KW <u>9.7</u> LB LIME/TON PR.: <u>91.0</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>669.6</u> TOT STM TO T/G: <u>2,820.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 19, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1389.0</u> KLB	STEAM PRODUCED: <u>1384.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1433.5</u> KLB	FEEDWATER USED: <u>1439.0</u> KLB	ENDING: <u>8680.0</u> WH TOT	BEGINNING: <u>181184</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8671.0</u> WH TOT	ENDING: <u>181184</u> CU FT
BLOWDOWN: <u>45</u> KLB	BLOWDOWN: <u>55</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.1</u> %	BLOWDOWN: <u>3.8</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2235500</u> JEM TOT	ENDING: <u>10.9</u> FT/IN OUT
ENDING: <u>74949.3</u> HRS	ENDING: <u>73945.8</u> HRS	BEGINNING: <u>2005760</u> JEM TOT	BEGINNING: <u>10.5</u> FT/IN OUT
BEGINNING: <u>74925.3</u> HRS	BEGINNING: <u>73921.8</u> HRS	TOTAL: <u>229.7</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>10.75</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>57.9</u> KLB/HR	AVG. STEAM FLOW: <u>57.7</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>216.5</u> TONS	APPROX REF PROC: <u>201.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>231.5</u> TONS	REFUSE PROCESSED: <u>230.7</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>29.5</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>69.9</u>	ENDING: <u>16</u> FT. OUT <u>25</u> IN OUT
TOTAL STEAM FLOW: <u>2773.0</u> KLB	GROSS REFUSE REC: <u>612.78</u> TONS		BEGINNING: <u>16</u> FT. OUT <u>30</u> IN OUT
TOTAL REFUSE PR. <u>421.5</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
<u>460.26</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>18.08</u>
WELL WATER USE:	TOTAL REFUSE REC: <u>612.78</u> TONS ✓	MEDICAL WASTE:	
ENDING: <u>424728000</u> GAL	EST PIT INVENTORY: <u>1,828.0</u> TONS	PROCESSED: <u>4.06</u> TONS	
BEGINNING: <u>424468000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>0.96</u> %	
TOTAL USED: <u>260000</u> GAL	<u>189.27</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>89.9</u> %	UNIT 2 % MCR: <u>89.5</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.7</u>	GROSS KW/TON PR. <u>614.9</u>	
NET KWH/TON PR. <u>545.0</u>	LB LIME/TON PR.: <u>3.0</u>	TOT STM TO T/G: <u>2,790.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 20, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1403.0</u> KLB	STEAM PRODUCED: <u>1398.8</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1448.3</u> KLB	FEEDWATER USED: <u>1461.4</u> KLB	ENDING: <u>8690.0</u> WH TOT	BEGINNING: <u>181184</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8680.0</u> WH TOT	ENDING: <u>181185</u> CU FT
BLOWDOWN: <u>45</u> KLB	BLOWDOWN: <u>63</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN %: <u>3.1</u> %	BLOWDOWN %: <u>4.3</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2466890</u> JEM TOT	ENDING: <u>11.6</u> FT/IN OUT
ENDING: <u>74973.3</u> HRS	ENDING: <u>73969.8</u> HRS	BEGINNING: <u>2235500</u> JEM TOT	BEGINNING: <u>10.9</u> FT/IN OUT
BEGINNING: <u>74949.3</u> HRS	BEGINNING: <u>73945.8</u> HRS	TOTAL: <u>231.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>11.50</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>58.5</u> KLB/HR	AVG. STEAM FLOW: <u>58.3</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>244.0</u> TONS	APPROX REF PROC: <u>217.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>233.8</u> TONS	REFUSE PROCESSED: <u>233.1</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>56.6</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>118.0</u>	ENDING: <u>15</u> FT. OUT <u>58</u> IN OUT
TOTAL STEAM FLOW: <u>2801.8</u> KLB	GROSS REFUSE REC: <u>563.78</u> TONS		BEGINNING: <u>16</u> FT. OUT <u>25</u> IN OUT
TOTAL REFUSE PR. <u>479.6</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
<u>485.46</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>19.83</u>
WELL WATER USE:	TOTAL REFUSE REC: <u>563.78</u> TONS ✓	MEDICAL WASTE:	
ENDING: <u>424989000</u> GAL	EST PIT INVENTORY: <u>1,575.0</u> TONS	PROCESSED: <u>18.56</u> TONS	
BEGINNING: <u>424728000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>3.87</u> %	
TOTAL USED: <u>261000</u> GAL	<u>296.21</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>90.8</u> %	UNIT 2 % MCR: <u>90.5</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.7</u>	GROSS KW/TON PR. <u>600.6</u>	
NET KWH/TON PR. <u>482.5</u>	LB LIME/TON PR.: <u>4.6</u>	TOT STM TO T/G: <u>2,807.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 21, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1393.2</u> KLB	STEAM PRODUCED: <u>1399.1</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1438.2</u> KLB	FEEDWATER USED: <u>1474.3</u> KLB	ENDING: <u>8700.0</u> WH TOT	BEGINNING: <u>181185</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8690.0</u> WH TOT	ENDING: <u>181185</u> CU FT
BLOWDOWN: <u>45</u> KLB	BLOWDOWN: <u>75</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.1</u> %	BLOWDOWN: <u>5.1</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>2898570</u> JEM TOT	ENDING: <u>7.4</u> FT/IN OUT
ENDING: <u>74997.3</u> HRS	ENDING: <u>73993.8</u> HRS	BEGINNING: <u>2466890</u> JEM TOT	BEGINNING: <u>11.6</u> FT/IN OUT
BEGINNING: <u>74973.3</u> HRS	BEGINNING: <u>73969.8</u> HRS	TOTAL: <u>231.7</u> MWH	RECEIVED: <u>24.80</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>7.33</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>58.0</u> KLB/HR	AVG. STEAM FLOW: <u>58.3</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>214.0</u> TONS	APPROX REF PROC: <u>204.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>232.2</u> TONS	REFUSE PROCESSED: <u>233.2</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>58.3</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>130.1</u>	ENDING: <u>15</u> FT. OUT <u>17</u> IN OUT
TOTAL STEAM FLOW: <u>2792.3</u> KLB	GROSS REFUSE REC: <u>588.73</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>58</u> IN OUT
TOTAL REFUSE PR. <u>433.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
	FERROUS HAULED: <u>35.64</u> TONS		EOM OUT: <u>16.42</u>
	TOTAL REFUSE REC: <u>553.09</u> TONS <u>552.79</u>	MEDICAL WASTE:	
WELL WATER USE:	EST PIT INVENTORY: <u>1,633.0</u> TONS	PROCESSED: <u>14.98</u> TONS	
ENDING: <u>425263000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>3.46</u> %	
BEGINNING: <u>424889000</u> GAL			
TOTAL USED: <u>274000</u> GAL	<u>206.92</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>90.1</u> %	UNIT 2 % MCR: <u>90.5</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.7</u>	GROSS KW/TON PR. <u>665.2</u>	
NET KWH/TON PR. <u>535.1</u>	LB LIME/TON PR.: <u>84.1</u>	TOT STM TO T/G: <u>2,812.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 22, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1406.3</u> KLB FEEDWATER USED: <u>1450.0</u> KLB	STEAM PRODUCED: <u>718.6</u> KLB FEEDWATER USED: <u>777.4</u> KLB	GENERATOR OUT: ENDING: <u>8707.0</u> WH TOT BEGINNING: <u>8700.0</u> WH TOT TOTAL: <u>201.6</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>181185</u> CU FT ENDING: <u>181250</u> CU FT TOTAL USED: <u>65</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>44</u> KLB BLOWDOWN: <u>3.0</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>59</u> KLB BLOWDOWN: <u>7.6</u> %	UTILITY OUT: ENDING: <u>2864000</u> JEM TOT BEGINNING: <u>2898570</u> JEM TOT TOTAL: <u>165.4</u> MWH	PEBBLE LIME: ENDING: <u>7.9</u> FT/IN OUT BEGINNING: <u>7.4</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>75021.3</u> HRS BEGINNING: <u>74997.3</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>74005.9</u> HRS BEGINNING: <u>73993.8</u> HRS TOTAL: <u>12.1</u> HRS	UTILITY IN: ENDING: <u>2727800</u> JEM TOT BEGINNING: <u>2727800</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>7.75</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>12.0</u> HRS	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>38.2</u> MWH KWH/TON: <u>123.7</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>134</u> LBS DAILY TOTAL: <u>403</u> LBS
AVG. STEAM FLOW: <u>58.6</u> KLB/HR	AVG. STEAM FLOW: <u>59.9</u> KLB/HR		CARBON INVENTORY: ENDING: <u>15</u> FT. OUT <u>7</u> IN OUT BEGINNING: <u>15</u> FT. OUT <u>17</u> IN OUT RECEIVED: <u>0.00</u> TONS
APPROX REF PROC: <u>196.2</u> TONS	APPROX REF PROC: <u>84.5</u> TONS		EOM OUT: <u>15.58</u>
REFUSE PROCESSED: <u>234.4</u> TONS	REFUSE PROCESSED: <u>119.8</u> TONS		
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2124.9</u> KLB TOTAL REFUSE PR. <u>292.4</u> TONS	GROSS REFUSE REC: <u>268.85</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>268.85</u> TONS ✓	MEDICAL WASTE: PROCESSED: <u>11.67</u> TONS % OF REFUSE PROC: <u>3.99</u> %	
WELL WATER USE: ENDING: <u>425481000</u> GAL BEGINNING: <u>425263000</u> GAL TOTAL USED: <u>218000</u> GAL	EST PIT INVENTORY: <u>2,031.0</u> TONS ✓ ASH HAULED: <u>0.00</u> TONS ✓		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>91.0</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>565.8</u>	UNIT 2 AVAILABILITY: <u>50.0</u> % UNIT 2 % MCR: <u>46.5</u> % LB STEAM/GROSS KW <u>10.5</u> LB LIME/TON PR.: <u>5.4</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>53.5</u> % GROSS KW/TON PR. <u>689.5</u> TOT STM TO T/G: <u>2,075.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#2 blr off line @ 1200 for discharger repairs.

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 23, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1431.2</u> KLB	STEAM PRODUCED: <u>629.8</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1475.3</u> KLB	FEEDWATER USED: <u>688.3</u> KLB	ENDING: <u>8714.0</u> WH TOT	BEGINNING: <u>181250</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8707.0</u> WH TOT	ENDING: <u>181578</u> CU FT
BLOWDOWN: <u>44</u> KLB	BLOWDOWN: <u>57</u> KLB	TOTAL: <u>201.6</u> MWH	TOTAL USED: <u>328</u> CU FT
BLOWDOWN: <u>3.0</u> %	BLOWDOWN: <u>8.2</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3012240</u> JEM TOT	ENDING: <u>8.4</u> FT/IN OUT
ENDING: <u>75045.3</u> HRS	ENDING: <u>74021.2</u> HRS	BEGINNING: <u>2864000</u> JEM TOT	BEGINNING: <u>7.9</u> FT/IN OUT
BEGINNING: <u>75021.3</u> HRS	BEGINNING: <u>74005.9</u> HRS	TOTAL: <u>148.2</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>15.3</u> HRS	UTILITY IN:	EOM OUT: <u>8.33</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>13.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>59.6</u> KLB/HR	AVG. STEAM FLOW: <u>48.4</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>218.4</u> TONS	APPROX REF PROC: <u>90.4</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>146</u> LBS
REFUSE PROCESSED: <u>238.5</u> TONS	REFUSE PROCESSED: <u>105.0</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>414</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>53.4</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>169.3</u>	ENDING: <u>15</u> FT. OUT <u>0</u> IN OUT
TOTAL STEAM FLOW: <u>2081.0</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS		BEGINNING: <u>15</u> FT. OUT <u>7</u> IN OUT
TOTAL REFUSE PR. <u>315.2</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
<u>347.7</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>15.00</u>
WELL WATER USE:	TOTAL REFUSE REC: <u>0.00</u> TONS ✓	MEDICAL WASTE:	
ENDING: <u>425694000</u> GAL	EST PIT INVENTORY: <u>1,517.0</u> TONS ✓	PROCESSED: <u>6.45</u> TONS	
BEGINNING: <u>425481000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	% OF REFUSE PROC: <u>2.05</u> %	
TOTAL USED: <u>213000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>54.2</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>92.6</u> %	UNIT 2 % MCR: <u>40.7</u> %	TG % MCR: <u>53.5</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>639.6</u>	
NET KWH/TON PR. <u>470.3</u>	LB LIME/TON PR.: <u>5.0</u>	TOT STM TO T/G: <u>1,854.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#2 blr off line for discharger repair, burner in #2 @ 0912.

Best Available Copy



OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 24, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1329.0</u> KLB FEEDWATER USED: <u>1372.0</u> KLB	STEAM PRODUCED: <u>1381.0</u> KLB FEEDWATER USED: <u>1438.0</u> KLB	GENERATOR OUT: ENDING: <u>8723.0</u> WH TOT BEGINNING: <u>8714.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>181578</u> CU FT ENDING: <u>181578</u> CU FT TOTAL USED: <u>0</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>43</u> KLB BLOWDOWN : <u>3.1</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>57</u> KLB BLOWDOWN : <u>4.0</u> %	UTILITY OUT: ENDING: <u>3231960</u> JEM TOT BEGINNING: <u>3012240</u> JEM TOT TOTAL: <u>219.7</u> MWH	PEBBLE LIME : ENDING: <u>9.2</u> FT/IN OUT BEGINNING: <u>8.4</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>75069.3</u> HRS BEGINNING: <u>75045.3</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>74045.2</u> HRS BEGINNING: <u>74021.2</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2727800</u> JEM TOT BEGINNING: <u>2727800</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>9.17</u>
BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>55.4</u> KLB/HR	BOILER RUN TIME: <u>24.0</u> HRS AVG. STEAM FLOW: <u>57.5</u> KLB/HR	GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>39.5</u> MWH KWH/TON: <u>88.9</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
APPROX REF PROC: <u>228.2</u> TONS REFUSE PROCESSED: <u>221.5</u> TONS	APPROX REF PROC: <u>201.6</u> TONS REFUSE PROCESSED: <u>230.2</u> TONS		CARBON INVENTORY: ENDING: <u>14</u> FT. OUT <u>53</u> IN OUT BEGINNING: <u>15</u> FT. OUT <u>0</u> IN OUT RECEIVED: <u>0.00</u> TONS EOM OUT: <u>18.42</u>
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			
TOTAL STEAM FLOW: <u>2710.0</u> KLB TOTAL REFUSE PR. <u>444.0</u> TONS	GROSS REFUSE REC: <u>862.01</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>862.01</u> TONS ✓	MEDICAL WASTE : PROCESSED: <u>14.18</u> TONS % OF REFUSE PROC: <u>3.19</u> %	
WELL WATER USE: ENDING: <u>425955000</u> GAL BEGINNING: <u>425894000</u> GAL TOTAL USED: <u>281000</u> GAL	EST PIT INVENTORY: <u>1,712.0</u> TONS ASH HAULED: <u>0.00</u> TONS <u>168.89</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>86.0</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>494.9</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>89.4</u> % LB STEAM/GROSS KW <u>10.5</u> LB LIME/TON PR.: <u>5.7</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>583.8</u> TOT STM TO T/G: <u>2,698.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

Best Available Copy

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 25, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1390.0</u> KLB	STEAM PRODUCED: <u>1408.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1435.0</u> KLB	FEEDWATER USED: <u>1490.0</u> KLB	ENDING: <u>8732.0</u> WH TOT	BEGINNING: <u>181578</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8723.0</u> WH TOT	ENDING: <u>181579</u> CU FT
BLOWDOWN: <u>45</u> KLB	BLOWDOWN: <u>82</u> KLB	TOTAL: <u>259.2</u> MWH	TOTAL USED: <u>1</u> CU FT
BLOWDOWN: <u>3.1</u> %	BLOWDOWN: <u>5.5</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3482350</u> JEM TOT	ENDING: <u>10.3</u> FT/IN OUT
ENDING: <u>75093.3</u> HRS	ENDING: <u>74069.0</u> HRS	BEGINNING: <u>3231960</u> JEM TOT	BEGINNING: <u>9.2</u> FT/IN OUT
BEGINNING: <u>75069.3</u> HRS	BEGINNING: <u>74045.2</u> HRS	TOTAL: <u>230.4</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>23.8</u> HRS		
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>10.25</u>
AVG. STEAM FLOW: <u>57.9</u> KLB/HR	AVG. STEAM FLOW: <u>58.7</u> KLB/HR	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
APPROX REF PROC: <u>168.3</u> TONS	APPROX REF PROC: <u>170.3</u> TONS	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
REFUSE PROCESSED: <u>231.7</u> TONS	REFUSE PROCESSED: <u>234.7</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2798.0</u> KLB	GROSS REFUSE REC: <u>804.75</u> TONS	IN PLANT USE: <u>28.8</u> MWH	CARBON INVENTORY:
TOTAL REFUSE PR. <u>338.6</u> TONS	NON PROCESSED: <u>0.00</u> TONS	KWH/TON: <u>85.1</u>	ENDING: <u>13</u> FT. OUT <u>97</u> IN OUT
	FERROUS HAULED: <u>0.00</u> TONS		BEGINNING: <u>14</u> FT. OUT <u>53</u> IN OUT
	TOTAL REFUSE REC: <u>804.75</u> TONS <u>798.30</u>		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	EST PIT INVENTORY: <u>2,120.0</u> TONS	MEDICAL WASTE:	EOM OUT: <u>21.08</u>
ENDING: <u>426219000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>0.00</u> TONS	
BEGINNING: <u>425955000</u> GAL		% OF REFUSE PROC: <u>0.00</u> %	
TOTAL USED: <u>264000</u> GAL	<u>181.45</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>89.9</u> %	UNIT 2 % MCR: <u>91.1</u> %	TG % MCR: <u>68.8</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.8</u>	GROSS KW/TON PR. <u>765.5</u>	
NET KWH/TON PR. <u>660.4</u>	LB LIME/TON PR.: <u>10.2</u>	TOT STM TO T/G: <u>2,821.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
 DATE May 26, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1388.0</u> KLB	STEAM PRODUCED: <u>1443.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1435.0</u> KLB	FEEDWATER USED: <u>1529.0</u> KLB	ENDING: <u>8742.0</u> WH TOT	BEGINNING: <u>181579</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8732.0</u> WH TOT	ENDING: <u>181579</u> CU FT
BLOWDOWN: <u>47</u> KLB	BLOWDOWN: <u>86</u> KLB	TOTAL: <u>286.0</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>3.3</u> %	BLOWDOWN: <u>5.6</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3695150</u> JEM TOT	ENDING: <u>6.5</u> FT/IN OUT
ENDING: <u>75117.3</u> HRS	ENDING: <u>74093.0</u> HRS	BEGINNING: <u>3462350</u> JEM TOT	BEGINNING: <u>10.3</u> FT/IN OUT
BEGINNING: <u>75093.3</u> HRS	BEGINNING: <u>74069.0</u> HRS	TOTAL: <u>232.8</u> MWH	RECEIVED: <u>24.60</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>6.42</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>57.8</u> KLB/HR	AVG. STEAM FLOW: <u>60.1</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>106.9</u> TONS	APPROX REF PROC: <u>99.5</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>231.3</u> TONS	REFUSE PROCESSED: <u>240.5</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>55.2</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2831.0</u> KLB	GROSS REFUSE REC: <u>534.45</u> TONS	KWH/TON: <u>257.8</u>	ENDING: <u>13</u> FT. OUT <u>63</u> IN OUT
TOTAL REFUSE PR. <u>214.1</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>13</u> FT. OUT <u>97</u> IN OUT
<u>477.0</u>	FERROUS HAULED: <u>18.93</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
	TOTAL REFUSE REC: <u>515.52</u> TONS <u>517.52</u>		EOM OUT: <u>18.25</u>
WELL WATER USE:	EST PIT INVENTORY: <u>2,140.0</u> TONS	MEDICAL WASTE:	
ENDING: <u>426523000</u> GAL	ASH HAULED: <u>0.00</u> TONS	PROCESSED: <u>7.77</u> TONS	
BEGINNING: <u>426219000</u> GAL	<u>142.90</u>	% OF REFUSE PROC: <u>3.63</u> %	
TOTAL USED: <u>304000</u> GAL			
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>89.8</u> %	UNIT 2 % MCR: <u>93.4</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.8</u>	GROSS KW/TON PR. <u>1345.0</u>	
NET KWH/TON PR. <u>1087.2</u>	LB LIME/TON PR.: <u>174.1</u>	TOT STM TO T/G: <u>2,849.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE May 27, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1453.0</u> KLB	STEAM PRODUCED: <u>1467.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1500.0</u> KLB	FEEDWATER USED: <u>1552.0</u> KLB	ENDING: <u>8752.0</u> WH TOT	BEGINNING: <u>181579</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8742.0</u> WH TOT	ENDING: <u>181589</u> CU FT
BLOWDOWN: <u>47</u> KLB	BLOWDOWN: <u>85</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>10</u> CU FT
BLOWDOWN: <u>3.1</u> %	BLOWDOWN: <u>5.5</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>3937650</u> JEM TOT	ENDING: <u>7.1</u> FT/IN OUT
ENDING: <u>75141.3</u> HRS	ENDING: <u>74117.0</u> HRS	BEGINNING: <u>3695150</u> JEM TOT	BEGINNING: <u>6.5</u> FT/IN OUT
BEGINNING: <u>75117.3</u> HRS	BEGINNING: <u>74093.0</u> HRS	TOTAL: <u>242.5</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>7.08</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2727800</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>60.5</u> KLB/HR	AVG. STEAM FLOW: <u>61.1</u> KLB/HR	BEGINNING: <u>2727800</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>164.0</u> TONS	APPROX REF PROC: <u>183.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>242.2</u> TONS	REFUSE PROCESSED: <u>244.5</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>45.5</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>127.5</u>	ENDING: <u>13</u> FT. OUT <u>43</u> IN OUT
TOTAL STEAM FLOW: <u>2920.0</u> KLB	GROSS REFUSE REC: <u>552.32</u> TONS		BEGINNING: <u>13</u> FT. OUT <u>63</u> IN OUT
TOTAL REFUSE PR. <u>356.8</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
<u>496.5</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		EOM OUT: <u>16.58</u>
WELL WATER USE:	TOTAL REFUSE REC: <u>552.32</u> TONS ✓	MEDICAL WASTE:	
ENDING: <u>426857000</u> GAL	EST PIT INVENTORY: <u>2,275.0</u> TONS	PROCESSED: <u>9.81</u> TONS	
BEGINNING: <u>426523000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.75</u> %	
TOTAL USED: <u>334000</u> GAL	<u>160.45</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>94.0</u> %	UNIT 2 % MCR: <u>94.9</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.1</u>	GROSS KW/TON PR. <u>807.2</u>	
NET KWH/TON PR. <u>679.6</u>	LB LIME/TON PR.: <u>5.3</u>	TOT STM TO T/G: <u>2,958.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 28 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1424.1</u> KLB FEEDWATER USED: <u>1471.0</u> KLB	STEAM PRODUCED: <u>1464.3</u> KLB FEEDWATER USED: <u>1494.3</u> KLB	GENERATOR OUT: ENDING: <u>8761.0</u> WH TOT BEGINNING: <u>8752.0</u> WH TOT TOTAL: <u>259.2</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>181689</u> CU FT ENDING: <u>181602</u> CU FT TOTAL USED: <u>13</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>47</u> KLB BLOWDOWN: <u>3.2</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>30</u> KLB BLOWDOWN: <u>2.0</u> %	UTILITY OUT: ENDING: <u>4105055</u> JEM TOT BEGINNING: <u>3937650</u> JEM TOT TOTAL: <u>167.4</u> MWH	PEBBLE LIME: ENDING: <u>7.7</u> FT/IN OUT BEGINNING: <u>7.1</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>75164.3</u> HRS BEGINNING: <u>75141.3</u> HRS TOTAL: <u>23.0</u> HRS	GRATE RUN TIME: ENDING: <u>74140.0</u> HRS BEGINNING: <u>74117.0</u> HRS TOTAL: <u>23.0</u> HRS	UTILITY IN: ENDING: <u>2731560</u> JEM TOT BEGINNING: <u>2727800</u> JEM TOT TOTAL: <u>3.8</u> MWH	EOM OUT: <u>7.58</u>
BOILER RUN TIME: <u>23.4</u> HRS AVG. STEAM FLOW: <u>61.0</u> KLB/HR APPROX REF PROC: <u>204.0</u> TONS	BOILER RUN TIME: <u>23.3</u> HRS AVG. STEAM FLOW: <u>62.7</u> KLB/HR APPROX REF PROC: <u>213.0</u> TONS	GENERATOR RUN TIME: <u>21.5</u> HRS IN PLANT USE: <u>95.6</u> MWH KWH/TON: <u>221.2</u>	CARBON USAGE: USAGE UNIT #1: <u>262</u> LBS USAGE UNIT #2: <u>261</u> LBS DAILY TOTAL: <u>523</u> LBS
REFUSE PROCESSED: <u>237.4</u> TONS	REFUSE PROCESSED: <u>244.1</u> TONS		CARBON INVENTORY: ENDING: <u>26</u> FT. OUT <u>66</u> IN OUT BEGINNING: <u>13</u> FT. OUT <u>43</u> IN OUT RECEIVED: <u>0.00</u> TONS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB			EOM OUT: <u>31.50</u>
TOTAL STEAM FLOW: <u>2888.4</u> KLB TOTAL REFUSE PR. <u>431.9</u> TONS	GROSS REFUSE REC: <u>213.00</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>0.00</u> TONS TOTAL REFUSE REC: <u>213.00</u> TONS	MEDICAL WASTE: PROCESSED: <u>14.89</u> TONS % OF REFUSE PROC: <u>3.45</u> %	
WELL WATER USE: ENDING: <u>427158000</u> GAL BEGINNING: <u>426857000</u> GAL TOTAL USED: <u>301000</u> GAL	EST PIT INVENTORY: <u>2,392.0</u> TONS ASH HAULED: <u>0.00</u> TONS		
UNIT 1 AVAILABILITY: <u>97.3</u> % UNIT 1 % MCR: <u>92.1</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>387.6</u>	UNIT 2 AVAILABILITY: <u>97.3</u> % UNIT 2 % MCR: <u>94.7</u> % LB STEAM/GROSS KW <u>11.1</u> LB LIME/TON PR.: <u>4.4</u>	TG AVAILABILITY: <u>89.6</u> % TG % MCR: <u>68.8</u> % GROSS KW/TON PR. <u>600.2</u> TOT STM TO T/G: <u>2,835.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

unit #1 down 25 mins unit #2 down 26 mins T/G down 2hrs 23 min electric *Storm*

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 29 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1501.9</u> KLB	STEAM PRODUCED: <u>1483.1</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1528.3</u> KLB	FEEDWATER USED: <u>1548.6</u> KLB	ENDING: <u>8771.0</u> WH TOT	BEGINNING: <u>181602</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8761.0</u> WH TOT	ENDING: <u>181608</u> CU FT
BLOWDOWN: <u>26</u> KLB	BLOWDOWN: <u>86</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>6</u> CU FT
BLOWDOWN: <u>1.7</u> %	BLOWDOWN: <u>5.5</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4395090</u> JEM TOT	ENDING: <u>8.2</u> FT/IN OUT
ENDING: <u>75188.3</u> HRS	ENDING: <u>74164.0</u> HRS	BEGINNING: <u>4159290</u> JEM TOT	BEGINNING: <u>7.7</u> FT/IN OUT
BEGINNING: <u>75164.3</u> HRS	BEGINNING: <u>74140.0</u> HRS	TOTAL: <u>235.8</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>8.17</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2731560</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>62.6</u> KLB/HR	AVG. STEAM FLOW: <u>61.0</u> KLB/HR	BEGINNING: <u>2731560</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>190.3</u> TONS	APPROX REF PROC: <u>212.7</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>250.3</u> TONS	REFUSE PROCESSED: <u>243.9</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>52.2</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>128.0</u>	ENDING: <u>26</u> FT. OUT <u>8</u> IN OUT
TOTAL STEAM FLOW: <u>2965.0</u> KLB	GROSS REFUSE REC: <u>224.20</u> TONS		BEGINNING: <u>26</u> FT. OUT <u>66</u> IN OUT
TOTAL REFUSE PR. <u>414.2</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
<i>505.7</i>	FERROUS HAULED: <u>0.00</u> TONS		EOM OUT: <u>26.67</u>
WELL WATER USE:	TOTAL REFUSE REC: <u>224.20</u> TONS <i>244.20</i>	MEDICAL WASTE:	
ENDING: <u>427461000</u> GAL	EST PIT INVENTORY: <u>2,217.0</u> TONS	PROCESSED: <u>11.18</u> TONS	
BEGINNING: <u>427158000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.70</u> %	
TOTAL USED: <u>303000</u> GAL	<i>76.86</i>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>97.2</u> %	UNIT 2 % MCR: <u>94.7</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.3</u>	GROSS KW/TON PR. <u>695.3</u>	
NET KWH/TON PR. <u>569.3</u>	LB LIME/TON PR.: <u>3.8</u>	TOT STM TO T/G: <u>2,994.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 30 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1473.0</u> KLB	STEAM PRODUCED: <u>1450.7</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1510.6</u> KLB	FEEDWATER USED: <u>1524.9</u> KLB	ENDING: <u>8781.0</u> WH TOT	BEGINNING: <u>181608</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8771.0</u> WH TOT	ENDING: <u>181613</u> CU FT
BLOWDOWN: <u>38</u> KLB	BLOWDOWN: <u>74</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>5</u> CU FT
BLOWDOWN %: <u>2.5</u> %	BLOWDOWN %: <u>4.9</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>4633360</u> JEM TOT	ENDING: <u>8.9</u> FT/IN OUT
ENDING: <u>75212.3</u> HRS	ENDING: <u>74188.0</u> HRS	BEGINNING: <u>4395090</u> JEM TOT	BEGINNING: <u>8.2</u> FT/IN OUT
BEGINNING: <u>75188.3</u> HRS	BEGINNING: <u>74164.0</u> HRS	TOTAL: <u>238.3</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>8.75</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2731560</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>61.4</u> KLB/HR	AVG. STEAM FLOW: <u>60.4</u> KLB/HR	BEGINNING: <u>2731560</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>275.1</u> TONS	APPROX REF PROC: <u>248.4</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>245.5</u> TONS	REFUSE PROCESSED: <u>241.8</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>48.7</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2823.7</u> KLB	GROSS REFUSE REC: <u>0.00</u> TONS	KWH/TON: <u>102.1</u>	ENDING: <u>25</u> FT. OUT <u>59</u> IN OUT
TOTAL REFUSE PR. <u>487.3</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>26</u> FT. OUT <u>8</u> IN OUT
WELL WATER USE:	FERROUS HAULED: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
ENDING: <u>427752000</u> GAL	TOTAL REFUSE REC: <u>0.00</u> TONS ✓	MEDICAL WASTE:	EOM OUT: <u>29.82</u>
BEGINNING: <u>427461000</u> GAL	EST PIT INVENTORY: <u>1,493.0</u> TONS	PROCESSED: <u>0.00</u> TONS	
TOTAL USED: <u>291000</u> GAL	ASH HAULED: <u>0.00</u> TONS ✓	% OF REFUSE PROC: <u>0.00</u> %	
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>95.3</u> %	UNIT 2 % MCR: <u>93.9</u> %	TG % MCR: <u>76.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.2</u>	GROSS KW/TON PR. <u>591.0</u>	
NET KWH/TON PR. <u>489.0</u>	LB LIME/TON PR.: <u>4.5</u>	TOT STM TO T/G: <u>2,924.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE MAY 31 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1430.3</u> KLB FEEDWATER USED: <u>1456.5</u> KLB	STEAM PRODUCED: <u>1447.1</u> KLB FEEDWATER USED: <u>1525.9</u> KLB	GENERATOR OUT: ENDING: <u>8791.0</u> WH TOT BEGINNING: <u>8781.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>181613</u> CU FT ENDING: <u>181619</u> CU FT TOTAL USED: <u>6</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>26</u> KLB BLOWDOWN: <u>1.8</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>79</u> KLB BLOWDOWN: <u>5.2</u> %	UTILITY OUT: ENDING: <u>4869800</u> JEM TOT BEGINNING: <u>4633360</u> JEM TOT TOTAL: <u>236.2</u> MWH	PEBBLE LIME: ENDING: <u>9.8</u> FT/IN OUT BEGINNING: <u>8.9</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>75236.3</u> HRS BEGINNING: <u>75212.3</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>74212.0</u> HRS BEGINNING: <u>74188.0</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2731560</u> JEM TOT BEGINNING: <u>2731560</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>9.67</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	AVG. STEAM FLOW: <u>59.6</u> KLB/HR	AVG. STEAM FLOW: <u>60.3</u> KLB/HR
APPROX REF PROC: <u>229.9</u> TONS	APPROX REF PROC: <u>216.2</u> TONS	REFUSE PROCESSED: <u>238.4</u> TONS	REFUSE PROCESSED: <u>241.2</u> TONS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>51.8</u> MWH KWH/TON: <u>116.0</u>	CARBON USAGE: USAGE UNIT #1: <u>269</u> LBS USAGE UNIT #2: <u>269</u> LBS DAILY TOTAL: <u>538</u> LBS
TOTAL STEAM FLOW: <u>2877.4</u> KLB TOTAL REFUSE PR. <u>448.1</u> TONS <u>479.6</u>	GROSS REFUSE REC: <u>315.96</u> TONS NON PROCESSED: <u>0.00</u> TONS <u>17.73</u> FERROUS HAULED: <u>0.00</u> TONS ✓ TOTAL REFUSE REC: <u>315.96</u> TONS <u>298.23</u>		CARBON INVENTORY: ENDING: <u>25</u> FT. OUT <u>39</u> IN OUT BEGINNING: <u>25</u> FT. OUT <u>59</u> IN OUT RECEIVED: <u>0.00</u> TONS
WELL WATER USE: ENDING: <u>428026000</u> GAL BEGINNING: <u>427752000</u> GAL TOTAL USED: <u>274000</u> GAL	EST PIT INVENTORY: <u>1,283.0</u> TONS ASH HAULED: <u>0.00</u> TONS ✓	MEDICAL WASTE: PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	EOM OUT: <u>28.25</u>
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>92.5</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>529.6</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>93.6</u> % LB STEAM/GROSS KW <u>10.0</u> LB LIME/TON PR.: <u>6.3</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>645.7</u> TOT STM TO T/G: <u>2,883.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

22 STM Totalizer o/s was in Calculated STM Flow Unit #1

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JUNE 1 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1444.0</u> KLB	STEAM PRODUCED: <u>1437.8</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1478.3</u> KLB	FEEDWATER USED: <u>1515.7</u> KLB	ENDING: <u>8801.0</u> WH TOT	BEGINNING: <u>181819</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8791.0</u> WH TOT	ENDING: <u>181624</u> CU FT
BLOWDOWN: <u>35</u> KLB	BLOWDOWN: <u>78</u> KLB	TOTAL: <u>288.0</u> MWH	TOTAL USED: <u>5</u> CU FT
BLOWDOWN: <u>2.4</u> %	BLOWDOWN: <u>5.1</u> %	UTILITY OUT:	PEBBLE LIME :
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>5107600</u> JEM TOT	ENDING: <u>10.8</u> FT/IN OUT
ENDING: <u>75260.3</u> HRS	ENDING: <u>74236.0</u> HRS	BEGINNING: <u>4869600</u> JEM TOT	BEGINNING: <u>9.8</u> FT/IN OUT
BEGINNING: <u>75236.3</u> HRS	BEGINNING: <u>74212.0</u> HRS	TOTAL: <u>238.0</u> MWH	RECEIVED: <u>0.00</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>10.67</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2731560</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>60.2</u> KLB/HR	AVG. STEAM FLOW: <u>59.9</u> KLB/HR	BEGINNING: <u>2731560</u> JEM TOT	USAGE UNIT #1: <u>269</u> LBS
APPROX REF PROC: <u>223.8</u> TONS	APPROX REF PROC: <u>210.4</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>269</u> LBS
REFUSE PROCESSED: <u>240.7</u> TONS	REFUSE PROCESSED: <u>239.6</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>538</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>50.0</u> MWH	CARBON INVENTORY:
TOTAL STEAM FLOW: <u>2881.8</u> KLB	GROSS REFUSE REC: <u>767.04</u> TONS	KWH/TON: <u>112.7</u>	ENDING: <u>25</u> FT. OUT <u>6</u> IN OUT
TOTAL REFUSE PR. <u>443.6</u> TONS	NON PROCESSED: <u>0.00</u> TONS		BEGINNING: <u>25</u> FT. OUT <u>39</u> IN OUT
<u>489.7</u>	FERROUS HAULED: <u>0.00</u> TONS ✓		RECEIVED: <u>0.00</u> TONS
WELL WATER USE:	TOTAL REFUSE REC: <u>767.04</u> TONS ✓	MEDICAL WASTE :	EOM OUT: <u>25.50</u>
ENDING: <u>428333000</u> GAL	EST PIT INVENTORY: <u>1,789.0</u> TONS	PROCESSED: <u>9.38</u> TONS	
BEGINNING: <u>428028000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>2.11</u> %	
TOTAL USED: <u>307000</u> GAL	<u>173.37</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>93.4</u> %	UNIT 2 % MCR: <u>93.0</u> %	TG % MCR: <u>78.4</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>10.0</u>	GROSS KW/TON PR. <u>649.2</u>	
NET KWH/TON PR. <u>538.5</u>	LB LIME/TON PR.: <u>7.1</u>	TOT STM TO T/G: <u>2,891.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

#1 STM Flow Totalizer Error STM Produce Calculated

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JUNE 2, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1461.0</u> KLB FEEDWATER USED: <u>1515.0</u> KLB	STEAM PRODUCED: <u>1467.0</u> KLB FEEDWATER USED: <u>1546.0</u> KLB	GENERATOR OUT: ENDING: <u>8811.0</u> WH TOT BEGINNING: <u>8801.0</u> WH TOT TOTAL: <u>288.0</u> MWH	NATURAL GAS USAGE: BEGINNING: <u>181624</u> CU FT ENDING: <u>181642</u> CU FT TOTAL USED: <u>18</u> CU FT
BOILER BLOWDOWN: BLOWDOWN: <u>54</u> KLB BLOWDOWN: <u>3.6</u> %	BOILER BLOWDOWN: BLOWDOWN: <u>79</u> KLB BLOWDOWN: <u>5.1</u> %	UTILITY OUT: ENDING: <u>5347410</u> JEM TOT BEGINNING: <u>5107600</u> JEM TOT TOTAL: <u>239.8</u> MWH	PEBBLE LIME : ENDING: <u>12.8</u> FT/IN OUT BEGINNING: <u>10.8</u> FT/IN OUT RECEIVED: <u>0.00</u> TONS
GRATE RUN TIME: ENDING: <u>75284.3</u> HRS BEGINNING: <u>75260.3</u> HRS TOTAL: <u>24.0</u> HRS	GRATE RUN TIME: ENDING: <u>74260.0</u> HRS BEGINNING: <u>74236.0</u> HRS TOTAL: <u>24.0</u> HRS	UTILITY IN: ENDING: <u>2731560</u> JEM TOT BEGINNING: <u>2731560</u> JEM TOT TOTAL: <u>0.0</u> MWH	EOM OUT: <u>12.67</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	AVG. STEAM FLOW: <u>60.9</u> KLB/HR	AVG. STEAM FLOW: <u>61.1</u> KLB/HR
APPROX REF PROC: <u>193.7</u> TONS	APPROX REF PROC: <u>208.3</u> TONS	REFUSE PROCESSED: <u>243.5</u> TONS	REFUSE PROCESSED: <u>244.5</u> TONS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		GENERATOR RUN TIME: <u>24.0</u> HRS IN PLANT USE: <u>48.2</u> MWH KWH/TON: <u>119.9</u>	CARBON USAGE: USAGE UNIT #1: <u>552</u> LBS USAGE UNIT #2: <u>552</u> LBS DAILY TOTAL: <u>1104</u> LBS
TOTAL STEAM FLOW: <u>2928.0</u> KLB TOTAL REFUSE PR. <u>402.0</u> TONS <i>4700</i>	GROSS REFUSE REC: <u>705.24</u> TONS NON PROCESSED: <u>0.00</u> TONS FERROUS HAULED: <u>18.98</u> TONS ✓ TOTAL REFUSE REC: <u>886.26</u> TONS ✓	EST PIT INVENTORY: <u>1,945.0</u> TONS ASH HAULED: <u>0.00</u> TONS <i>192.35</i>	CARBON INVENTORY: ENDING: <u>24</u> FT. OUT <u>66</u> IN OUT BEGINNING: <u>25</u> FT. OUT <u>6</u> IN OUT RECEIVED: <u>0.00</u> TONS
WELL WATER USE: ENDING: <u>428646000</u> GAL BEGINNING: <u>428333000</u> GAL TOTAL USED: <u>313000</u> GAL		MEDICAL WASTE : PROCESSED: <u>0.00</u> TONS % OF REFUSE PROC: <u>0.00</u> %	EOM OUT: <u>29.50</u>
UNIT 1 AVAILABILITY: <u>100.0</u> % UNIT 1 % MCR: <u>94.5</u> % LB STEAM/LB PR. <u>3.0</u> NET KWH/TON PR. <u>596.5</u>	UNIT 2 AVAILABILITY: <u>100.0</u> % UNIT 2 % MCR: <u>94.9</u> % LB STEAM/GROSS KW <u>10.2</u> LB LIME/TON PR.: <u>15.6</u>	TG AVAILABILITY: <u>100.0</u> % TG % MCR: <u>76.4</u> % GROSS KW/TON PR. <u>716.4</u> TOT STM TO T/G: <u>2,942.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)

OGDEN MARTIN SYSTEMS OF LAKE, INC.
DAILY PRODUCTION REPORT
DATE JUNE 3, 1999

BOILER NO. 1	BOILER NO. 2	ELECTRICITY	INVENTORY
STEAM PRODUCED: <u>1549.0</u> KLB	STEAM PRODUCED: <u>1537.0</u> KLB	GENERATOR OUT:	NATURAL GAS USAGE:
FEEDWATER USED: <u>1553.0</u> KLB	FEEDWATER USED: <u>1614.0</u> KLB	ENDING: <u>8822.0</u> WH TOT	BEGINNING: <u>181642</u> CU FT
BOILER BLOWDOWN:	BOILER BLOWDOWN:	BEGINNING: <u>8811.0</u> WH TOT	ENDING: <u>181642</u> CU FT
BLOWDOWN: <u>4</u> KLB	BLOWDOWN: <u>77</u> KLB	TOTAL: <u>316.8</u> MWH	TOTAL USED: <u>0</u> CU FT
BLOWDOWN: <u>0.3</u> %	BLOWDOWN: <u>4.8</u> %	UTILITY OUT:	PEBBLE LIME:
GRATE RUN TIME:	GRATE RUN TIME:	ENDING: <u>5599410</u> JEM TOT	ENDING: <u>7.3</u> FT/IN OUT
ENDING: <u>75308.3</u> HRS	ENDING: <u>74284.0</u> HRS	BEGINNING: <u>5347410</u> JEM TOT	BEGINNING: <u>12.8</u> FT/IN OUT
BEGINNING: <u>75284.3</u> HRS	BEGINNING: <u>74260.0</u> HRS	TOTAL: <u>252.0</u> MWH	RECEIVED: <u>25.09</u> TONS
TOTAL: <u>24.0</u> HRS	TOTAL: <u>24.0</u> HRS	UTILITY IN:	EOM OUT: <u>7.25</u>
BOILER RUN TIME: <u>24.0</u> HRS	BOILER RUN TIME: <u>24.0</u> HRS	ENDING: <u>2731560</u> JEM TOT	CARBON USAGE:
AVG. STEAM FLOW: <u>64.5</u> KLB/HR	AVG. STEAM FLOW: <u>64.0</u> KLB/HR	BEGINNING: <u>2731560</u> JEM TOT	USAGE UNIT #1: <u>552</u> LBS
APPROX REF PROC: <u>220.0</u> TONS	APPROX REF PROC: <u>197.0</u> TONS	TOTAL: <u>0.0</u> MWH	USAGE UNIT #2: <u>552</u> LBS
REFUSE PROCESSED: <u>258.2</u> TONS	REFUSE PROCESSED: <u>258.2</u> TONS	GENERATOR RUN TIME: <u>24.0</u> HRS	DAILY TOTAL: <u>1104</u> LBS
NOTE: REFUSE PROCESSED BASED ON STEAM FLOW AND REFUSE @ 5000 BTU/LB		IN PLANT USE: <u>64.8</u> MWH	CARBON INVENTORY:
		KWH/TON: <u>149.3</u>	ENDING: <u>24</u> FT. OUT <u>17</u> IN OUT
TOTAL STEAM FLOW: <u>3086.0</u> KLB	GROSS REFUSE REC: <u>717.86</u> TONS		BEGINNING: <u>24</u> FT. OUT <u>66</u> IN OUT
TOTAL REFUSE PR. <u>434.0</u> TONS	NON PROCESSED: <u>0.00</u> TONS		RECEIVED: <u>0.00</u> TONS
<u>531.4</u>	FERROUS HAULED: <u>19.27</u> TONS ✓		EOM OUT: <u>25.42</u>
WELL WATER USE:	TOTAL REFUSE REC: <u>698.59</u> TONS <u>681.44</u>	MEDICAL WASTE:	
ENDING: <u>428953000</u> GAL	EST PIT INVENTORY: <u>2,276.0</u> TONS	PROCESSED: <u>16.98</u> TONS	
BEGINNING: <u>428646000</u> GAL	ASH HAULED: <u>0.00</u> TONS	% OF REFUSE PROC: <u>3.91</u> %	
TOTAL USED: <u>307000</u> GAL	<u>238.83</u>		
UNIT 1 AVAILABILITY: <u>100.0</u> %	UNIT 2 AVAILABILITY: <u>100.0</u> %	TG AVAILABILITY: <u>100.0</u> %	
UNIT 1 % MCR: <u>100.2</u> %	UNIT 2 % MCR: <u>99.4</u> %	TG % MCR: <u>84.1</u> %	
LB STEAM/LB PR. <u>3.0</u>	LB STEAM/GROSS KW <u>9.7</u>	GROSS KW/TON PR. <u>730.0</u>	
NET KWH/TON PR. <u>580.7</u>	LB LIME/TON PR.: <u>75.8</u>	TOT STM TO T/G: <u>3,078.0</u>	

EQUIPMENT OUT OF SERVICE (HOURS AND REASON)
