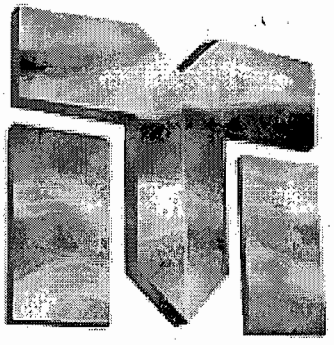

TRANSMONTAIGNE INC.

Delivering America's Fuel Supply, on Demand

Cape Canaveral
Coastal Fuels Marketing Inc.

Title V Permit Application

Coastal Fuels Marketing, Inc.
A SUBSIDIARY OF TRANSMONTAIGNE

Renewal due October 7, 2003
Application - Permit Expires April 7, 2004

October 9, 2003

Mr. Alan Zahm
Florida Department of Environmental Protection
3319 Maguire Boulevard, Suite 232
Orlando, Florida 32803

Re: CAM Plan for Title V Renewal
Cape Canaveral Terminal (Permit No. 0090029-003-AV)
Coastal Fuels Marketing Inc.

Dear Mr. Zahm,

Coastal Fuels Marketing Inc. (CFMI) owns and operates the Cape Canaveral Terminal, located in Cape Canaveral, Florida. The Title V permit, which this facility operates under, is currently being renewed. Please find attached the Compliance Assurance Monitoring (CAM) Plan for the Cape Canaveral Title V.

If you have any questions, or need further information, please call me at (303) 626-8209.

Sincerely,

COASTAL FUELS MARKETING INC.

Garrett Clemons

Garrett Clemons
Environmental Analyst
Regulatory Compliance

Flare Monitoring	**Indicator No. 1**
I. Indicator	Presence of Flame
Monitoring Approach	Flame presence is monitored using a thermocouple. {Operations Note. After a tanker truck is hooked up at the loading rack, a remote signal is sent to the flare programmable logic controller (PLC) to automatically ignite the pilot flame. A trial for ignition period is started and continues for 5 minutes or until the thermocouple is proven. During this time the pilot gas solenoid and flame front generator solenoid are held open. When the pilot has proven, a permit to load signal is given to the load rack resulting in a permissive position. The RCM elctro-hydraulic fail-safe actuator receives the same permit to load signal and opens up a hydraulic valve that allows the vapors to proceed to the ignitor.
II. Indicator Range	A loss of the permissive will occur during loading if the thermocoupler's temperature switch goes below its set point resulting in an automatic shutoff at the loading rack making loading impossible.
III. Performance Criteria	
A. Data Representativeness	The thermocoupler is positioned within the stack to detect the presence of the flame.
B. Verification of Operational Status	A green light in operator's office is on whenever the thermocoupler detects the presence of a flame.
C. QA/QC Practices and Criteria	Manufacturer's routine maintenance requirements include keeping the flame detection system adjusted for the smoothest, most reliable operation, and ensuring that the flame signal current is above the manufacturer's minimum acceptable level.
D. Monitoring Frequency	The thermocoupler operates continuously, when the flare is operating.
E. Data Collection Procedures	The thermocoupler continually monitors the flame and sends a permissive signal to the logic panel.
F. Averaging Period	NA

46 TPY after Control

Coastal Fuels Marketing, Inc.
A SUBSIDIARY OF TRANSMONTAIGNE

October 7, 2003

Mr. Alan Zahm
Florida Department of Environmental Protection
3319 Maguire Boulevard, Suite 232
Orlando, Florida 32803

Re: Title V Permit Renewal
Cape Canaveral Terminal
Coastal Fuels Marketing Inc.

Dear Mr. Zahm,

Coastal Fuels Marketing Inc. (CFMI) owns and operates the Cape Canaveral Terminal, located in Cape Canaveral, Florida. The terminal is operating in accordance with Title V permit No. 0090029-003-AV.

This Title V permit will expire on April 4, 2004. Please find enclosed the Title V permit renewal application for the Cape Canaveral Terminal. The permit can be renewed as it is currently written, with two exceptions. Boiler No. 1 is no longer in operation, therefore, can be taken out of the permit. Heater Nos. 5 and 6 should be referred to as 4 and 5.

Also included with the permit application is the emissions test report for the Zeeco flare, as well as the VE test report for Boiler No. 2. If you have any questions, or need further information, please call me at (303) 626-8209.

Sincerely,

COASTAL FUELS MARKETING INC.

Garrett Clemons
Environmental Analyst
Regulatory Compliance

cc: Mr. Richard Vogel, CFMI
Mr. Rex Thompson, CFMI

Table of Contents

Department of
Environmental Protection

Division of Air Resource Management

APPLICATION FOR AIR PERMIT - LONG FORM

I. APPLICATION INFORMATION

Air Construction Permit – Use this form to apply for an air construction permit for a proposed project:

- subject to prevention of significant deterioration (PSD) review, nonattainment area (NAA) new source review, or maximum achievable control technology (MACT) review; or
- where the applicant proposes to assume a restriction on the potential emissions of one or more pollutants to escape a federal program requirement such as PSD review, NAA new source review, Title V, or MACT; or
- at an existing federally enforceable state air operation permit (FESOP) or Title V permitted facility.

Air Operation Permit – Use this form to apply for:

- an initial federally enforceable state air operation permit (FESOP); or
- an initial/revised/renewal Title V air operation permit.

Air Construction Permit & Revised/Renewal Title V Air Operation Permit (Concurrent Processing Option) – Use this form to apply for both an air construction permit and a revised or renewal Title V air operation permit incorporating the proposed project.

To ensure accuracy, please see form instructions.

Identification of Facility

1. Facility Owner/Company Name: Coastal Fuels Marketing Inc.
2. Site Name: Cape Canaveral
3. Facility Identification Number: 0090029-003-AV
4. Facility Location:
   Street Address or Other Locator: 8952 North Atlantic Avenue
   City: Cape Canaveral County: Zip Code: 32920
5. Relocatable Facility? ☐ Yes ☒ No
6. Existing Title V Permitted Facility? ☒ Yes ☐ No

Application Contact

1. Application Contact Name: Garrett Clemons
2. Application Contact Mailing Address.
   Organization/Firm: TransMontaigne Product Services Inc.
   Street Address: P.O. Box 5660
   City: Denver State: CO Zip Code: 80217
3. Application Contact Telephone Numbers...
   Telephone: (303) 626 -8209 ext. Fax: (303)626-8228
4. Application Contact Email Address:

Application Processing Information (DEP Use)

1. Date of Receipt of Application:	
2. Project Number(s):	
3. PSD Number (if applicable):	
4. Siting Number (if applicable):	

APPLICATION INFORMATION

Purpose of Application

This application for air permit is submitted to obtain: (Check one)

Air Construction Permit

☐ Air construction permit.

Air Operation Permit

☐ Initial Title V air operation permit.

☐ Title V air operation permit revision.

☒ Title V air operation permit renewal.

☐ Initial federally enforceable state air operation permit (FESOP) where professional engineer (PE) certification is required.

☐ Initial federally enforceable state air operation permit (FESOP) where professional engineer (PE) certification is not required.

Air Construction Permit and Revised/Renewal Title V Air Operation Permit (Concurrent Processing)

☐ Air construction permit and Title V permit revision, incorporating the proposed project.

☐ Air construction permit and Title V permit renewal, incorporating the proposed project.

Note: By checking one of the above two boxes, you, the applicant, are requesting concurrent processing pursuant to Rule 62-213.405, F.A.C. In such case, you must also check the following box:

☐ I hereby request that the department waive the processing time requirements of the air construction permit to accommodate the processing time frames of the Title V air operation permit.

Application Comment

This is the Title V permit renewal application for permit # 0090029-003-AV.

APPLICATION INFORMATION

Scope of Application

Emissions Unit ID Number	Description of Emissions Unit	Air Permit Type	Air Permit Proc. Fee
002	Steam Boiler No. 2		
024	Asphalt Heaters No. 5 and No. 6		
025	Fourteen Petroleum Storage Tanks		
026	Five Petroleum Storage Tanks		
006	South Gasoline Loading Rack		
019	North Loading Rack, Asphalt Loading Rack, Marine Loading/Unloading and Vessel Bunkering, and Fugitive Emisisons from Valves, Flanges, Fittings, Pumps, Etc.		

Application Processing Fee

Check one: ☐ Attached - Amount: $_____ ☒ Not Applicable

APPLICATION INFORMATION

Application Responsible Official Certification

Complete if applying for an initial/revised/renewal Title V permit or concurrent processing of an air construction permit and a revised/renewal Title V permit. If there are multiple responsible officials, the "application responsible official" need not be the "primary responsible official."

1. Application Responsible Official Name: Dudley Tarlton

2. Application Responsible Official Qualification (Check one or more of the following options, as applicable):

   [X] For a corporation, the president, secretary, treasurer, or vice-president of the corporation in charge of a principal business function, or any other person who performs similar policy or decision-making functions for the corporation, or a duly authorized representative of such person if the representative is responsible for the overall operation of one or more manufacturing, production, or operating facilities applying for or subject to a permit under Chapter 62-213, F.A.C.

   [ ] For a partnership or sole proprietorship, a general partner or the proprietor, respectively.

   [ ] For a municipality, county, state, federal, or other public agency, either a principal executive officer or ranking elected official.

   [ ] The designated representative at an Acid Rain source.

3. Application Responsible Official Mailing Address...
   Organization/Firm: TransMontaigne Product Services Inc.
   Street Address: P.O. Box 5660
   City: Denver State: CO Zip Code: 80217

4. Application Responsible Official Telephone Numbers...
   Telephone: (303) 626-8200 ext. Fax: ( ) -

5. Application Responsible Official Email Address:

6. Application Responsible Official Certification:

   I, the undersigned, am a responsible official of the Title V source addressed in this air permit application. I hereby certify, based on information and belief formed after reasonable inquiry, that the statements made in this application are true, accurate and complete and that, to the best of my knowledge, any estimates of emissions reported in this application are based upon reasonable techniques for calculating emissions. The air pollutant emissions units and air pollution control equipment described in this application will be operated and maintained so as to comply with all applicable standards for control of air pollutant emissions found in the statutes of the State of Florida and rules of the Department of Environmental Protection and revisions thereof and all other applicable requirements identified in this application to which the Title V source is subject. I understand that a permit, if granted by the department, cannot be transferred without authorization from the department, and I will promptly notify the department upon sale or legal transfer of the facility or any permitted emissions unit. Finally, I certify that the facility and each emissions unit are in compliance with all applicable requirements to which they are subject, except as identified in compliance plan(s) submitted with this application.

Signature _____ Date 10/7/03

II. FACILITY INFORMATION

A. GENERAL FACILITY INFORMATION

Facility Location and Type

1. Facility UTM Coordinates... Zone 17 East (km) 538.98 North (km) 3141.99		2. Facility Latitude/Longitude... Latitude (DD/MM/SS) 28 24 24 Longitude (DD/MM/SS) 80 36 9	
3. Governmental Facility Code: 0	4. Facility Status Code: A	5. Facility Major Group SIC Code:	6. Facility SIC(s): 4226
7. Facility Comment :			

Facility Contact

1. Facility Contact Name: Craig Smith
2. Facility Contact Mailing Address... Organization/Firm: Coastal Fuels Marketing Inc. Street Address: 8954 North Atlantic Ave City: Cape Canaveral State: FL Zip Code: 32920
3. Facility Contact Telephone Numbers: Telephone: (321) 783-3393 ext. Fax: ( ) -
4. Facility Contact Email Address:

Facility Primary Responsible Official

Complete if an "application responsible official" is identified in Section I. that is not the facility "primary responsible official."

1. Facility Primary Responsible Official Name: Craig Smith
2. Facility Primary Responsible Official Mailing Address... Organization/Firm: Same as Above Street Address: City: State: Zip Code:
3. Facility Primary Responsible Official Telephone Numbers... Telephone: ( ) - ext. Fax: ( ) -
4. Facility Primary Responsible Official Email Address:

FACILITY INFORMATION

Facility Regulatory Classifications

Check all that would apply *following* completion of all projects and implementation of all other changes proposed in this application for air permit. Refer to instructions to distinguish between a "major source" and a "synthetic minor source."

1. ☐ Small Business Stationary Source	☐ Unknown
2. ☐ Synthetic Non-Title V Source	
3. ☒ Title V Source	
4. ☒ Major Source of Air Pollutants, Other than Hazardous Air Pollutants (HAPs)	
5. ☐ Synthetic Minor Source of Air Pollutants, Other than HAPs	
6. ☐ Major Source of Hazardous Air Pollutants (HAPs)	
7. ☒ Synthetic Minor Source of HAPs	
8. ☒ One or More Emissions Units Subject to NSPS (40 CFR Part 60)	
9. ☐ One or More Emissions Units Subject to Emission Guidelines (40 CFR Part 60)	
10. ☐ One or More Emissions Units Subject to NESHAP (40 CFR Part 61 or Part 63)	
11. ☒ Title V Source Solely by EPA Designation (40 CFR 70.3(a)(5))	
12. Facility Regulatory Classifications Comment:	

FACILITY INFORMATION

List of Pollutants Emitted by Facility

1. Pollutant Emitted	2. Pollutant Classification	3. Emissions Cap [Y or N]?
VOC	NA	< 250
HAPS	SM	< 25
H017	SM	< 10
H053	SM	< 10
H085	SM	< 10
H104	SM	< 10
H169	SM	< 10
H181	SM	< 10
H186	SM	< 10

B. EMISSIONS CAPS

Facility-Wide or Multi-Unit Emissions Caps

1. Pollutant Subject to Emissions Cap	2. Facility Wide Cap [Y or N]? (all units)	3. Emissions Unit ID No.s Under Cap (if not all units)	4. Hourly Cap (lb/hr)	5. Annual Cap (ton/yr)	6. Basis for Emissions Cap
VOC				< 250	
HAPS				< 25	ESCTIII
H017				< 10	ESCTIII
H053				< 10	ESCTIII
H085				< 10	ESCTIII
H104				< 10	ESCTIII
H169				< 10	ESCTIII
H181				< 10	ESCTIII
H186				< 10	ESCTIII

FACILITY INFORMATION

7. Facility-Wide or Multi-Unit Emissions Cap Comment:

C. FACILITY ADDITIONAL INFORMATION

Additional Requirements for All Applications, Except as Otherwise Stated

1. Facility Plot Plan: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)
   ☐ Attached, Document ID:_____ ☒ Previously Submitted, Date:_____
2. Process Flow Diagram(s): (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)
   ☐ Attached, Document ID:_____ ☒ Previously Submitted, Date:_____
3. Precautions to Prevent Emissions of Unconfined Particulate Matter: (Required for all permit applications, except Title V air operation permit revision applications if this information was submitted to the department within the previous five years and would not be altered as a result of the revision being sought)
   ☐ Attached, Document ID:_____ ☒ Previously Submitted, Date:_____

Additional Requirements for Air Construction Permit Applications

1. Area Map Showing Facility Location:
   ☐ Attached, Document ID:_____ ☐ Not Applicable (existing permitted facility)
2. Description of Proposed Construction or Modification:
   ☐ Attached, Document ID:_____
3. Rule Applicability Analysis:
   ☐ Attached, Document ID:_____
4. List of Exempt Emissions Units (Rule 62-210.300(3)(a) or (b)1., F.A.C.):
   ☐ Attached, Document ID:_____ ☐ Not Applicable (no exempt units at facility)
5. Fugitive Emissions Identification (Rule 62-212.400(2), F.A.C.):
   ☐ Attached, Document ID:_____ ☐ Not Applicable
6. Preconstruction Air Quality Monitoring and Analysis (Rule 62-212.400(5)(f), F.A.C.):
   ☐ Attached, Document ID:_____ ☐ Not Applicable
7. Ambient Impact Analysis (Rule 62-212.400(5)(d), F.A.C.):
   ☐ Attached, Document ID:_____ ☐ Not Applicable
8. Air Quality Impact since 1977 (Rule 62-212.400(5)(h)5., F.A.C.):
   ☐ Attached, Document ID:_____ ☐ Not Applicable
9. Additional Impact Analyses (Rules 62-212.400(5)(e)1. and 62-212.500(4)(e), F.A.C.):
   ☐ Attached, Document ID:_____ ☐ Not Applicable
10. Alternative Analysis Requirement (Rule 62-212.500(4)(g), F.A.C.):
    ☐ Attached, Document ID:_____ ☐ Not Applicable

FACILITY INFORMATION

Additional Requirements for FESOP Applications

1. List of Exempt Emissions Units (Rule 62-210.300(3)(a) or (b)1., F.A.C.):
   ☐ Attached, Document ID:_____ ☐ Not Applicable (no exempt units at facility)

Additional Requirements for Title V Air Operation Permit Applications

1. List of Insignificant Activities (Required for initial/renewal applications only):
   ☒ Attached, Document ID:_____ ☐ Not Applicable (revision application)

2. Identification of Applicable Requirements (Required for initial/renewal applications, and for revision applications if this information would be changed as a result of the revision being sought):
   ☒ Attached, Document ID:_____
   ☐ Not Applicable (revision application with no change in applicable requirements)

3. Compliance Report and Plan (Required for all initial/revision/renewal applications):
   ☐ Attached, Document ID:_____
   Note: A compliance plan must be submitted for each emissions unit that is not in compliance with all applicable requirements at the time of application and/or at any time during application processing. The department must be notified of any changes in compliance status during application processing.

4. List of Equipment/Activities Regulated under Title VI (If applicable, required for initial/renewal applications only):
   ☐ Attached, Document ID:_____
   ☐ Equipment/Activities On site but Not Required to be Individually Listed
   ☒ Not Applicable

5. Verification of Risk Management Plan Submission to EPA (If applicable, required for initial/renewal applications only) :
   ☐ Attached, Document ID:_____ ☒ Not Applicable

6. Requested Changes to Current Title V Air Operation Permit:
   ☒ Attached, Document ID:_____ ☐ Not Applicable

Additional Requirements Comment

III. EMISSIONS UNIT INFORMATION

A. TYPE OF EMISSIONS UNIT
(Regulated and Unregulated Emissions Units)

Emissions Unit Information Section 1

General VOC Storage Tanks & NLR/ALR

Type of Emissions Unit Addressed in This Section

1. Regulated or Unregulated Emissions Unit? Check one :

[X] The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.

[ ] The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.

2. Single Process, Group of Processes, or Fugitive Only? Check one :

[ ] This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).

[X] This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.

[ ] This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only.

Emissions Unit Information Section 1

B. GENERAL EMISSIONS UNIT INFORMATION
(Regulated and Unregulated Emissions Units)

Emissions Unit Description and Status

1. Description of Emissions Unit Addressed in This Section : General VOC Storage Tanks & NLR/ALR		
2. Emissions Unit Identification Number : [ ] No Corresponding ID [X] Unknown		
3. Emissions Unit Status Code : A	4. Acid Rain Unit? [ ] Yes [X] No	5. Emissions Unit Major Group SIC Code : 51
6. Emissions Unit Comment : The VOC emission sources covered under this emission unit consist of 2 storage tanks subject to the General VOC regulations: Tank nos. 9 and 15. Pursuant to the current construction permit a dome has been installed on the external floating roof tank no. 15. This construction modification application reflects an increased throughput. See attachment EU1-1 for details of the tank. This application also reflects an increase in throughput through the NLR and ALR, tank no. 2 may also store diesel, changes in throughput in fixed roof tank nos 7, 12, and 13. See attachment EU1-1 for details of the tank.		

Emissions Unit Information Section 1
General VOC Storage Tanks & NLR/ALR

Emissions Unit Control Equipment 1

1. Description : VOC controls on storage tank no. 9 consisting of an internal floating roof with both primary and secondary seals. VOC controls on storage tank no. 15 consisting of an external floating roof with dome and both primary and secondary seals.
2. Control Device or Method Code : 99

C. EMISSIONS UNIT DETAIL INFORMATION
(Regulated Emissions Units Only)

Emissions Unit Information Section 1
General VOC Storage Tanks & NLR/ALR

Emissions Unit Details

1. Initial Startup Date :		
2. Long-term Reserve Shutdown Date :		
3. Package Unit : Manufacturer :		Model Number :
4. Generator Nameplate Rating :	MW	
5. Incinerator Information : Dwell Temperature : Dwell Time : Incinerator Afterburner Temperature :		 Degrees Fahrenheit Seconds Degrees Fahrenheit

Emissions Unit Operating Capacity

1. Maximum Heat Input Rate :	mmBtu/hr	
2. Maximum Incinerator Rate :	lb/hr	tons/day
3. Maximum Process or Throughput Rate :		
4. Maximum Production Rate :		
5. Operating Capacity Comment :		

Emissions Unit Operating Schedule

Requested Maximum Operating Schedule :		
	24 hours/day	7 days/week
	52 weeks/year	8,760 hours/year

D. EMISSIONS UNIT REGULATIONS
(Regulated Emissions Units Only)

Emissions Unit Information Section 1
General VOC Storage Tanks & NLR/ALR

Rule Applicability Analysis

See attached list.

List of Applicable Regulations

62-296.320(1) - General VOC Regulations

E. EMISSION POINT (STACK/VENT) INFORMATION

Emissions Unit Information Section _____

Emission Point Description and Type :

1. Identification of Point on Plot Plan or Flow Diagram :	
2. Emission Point Type Code :	
3. Descriptions of Emission Points Comprising this Emissions Unit :	
4. ID Numbers or Descriptions of Emission Units with this Emission Point in Common :	
5. Discharge Type Code :	
6. Stack Height :	feet
7. Exit Diameter :	feet
8. Exit Temperature :	°F
9. Actual Volumetric Flow Rate :	acfm
10. Percent Water Vapor :	%
11. Maximum Dry Standard Flow Rate :	dscfm
12. Nonstack Emission Point Height :	feet
13. Emission Point UTM Coordinates :	
Zone : East (km) :	North (km) :
14. Emission Point Comment :	

F. SEGMENT (PROCESS/FUEL) INFORMATION

Emissions Unit Information Section 1

General VOC Storage Tanks & NLR/ALR

Segment Description and Rate : Segment 1

1. Segment Description (Process/Fuel Type and Associated Operating Method/Mode) : External Floating Roof Storage Tank - With Primary and Secondary Seals - Gasoline with an average RVP of 11.5 stored	
2. Source Classification Code (SCC) : 4-04-001-49	
3. SCC Units : Thousand Gallons Transferred or Handled	
4. Maximum Hourly Rate :	5. Maximum Annual Rate : 39,900.00
6. Estimated Annual Activity Factor :	
7. Maximum Percent Sulfur :	8. Maximum Percent Ash :
9. Million Btu per SCC Unit :	
10. Segment Comment : This SCC cover storage tank no. 15	

F. SEGMENT (PROCESS/FUEL) INFORMATION

Emissions Unit Information Section 1

General VOC Storage Tanks & NLR/ALR

Segment Description and Rate : Segment 2

1. Segment Description (Process/Fuel Type and Associated Operating Method/Mode) : *Internal Floating Roof Storage Tank - With Primary and Secondary Seals* Gasoline with an average RVP of 11.5 stored	
2. Source Classification Code (SCC) : 4-04-001-79	
3. SCC Units : Thousand Gallons Transferred or Handled	
4. Maximum Hourly Rate :	5. Maximum Annual Rate : 31,500.00
6. Estimated Annual Activity Factor :	
7. Maximum Percent Sulfur :	8. Maximum Percent Ash :
9. Million Btu per SCC Unit :	
10. Segment Comment : This SCC covers Tank No. 9	

G. EMISSIONS UNIT POLLUTANTS
(Regulated and Unregulated Emissions Units)

Emissions Unit Information Section 1
General VOC Storage Tanks & NLR/ALR

1. Pollutant Emitted	2. Primary Control Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
1 - VOC	099		WP

H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION
(Regulated Emissions Units Only - Emissions Limited Pollutants Only)

Emissions Unit Information Section 1
General VOC Storage Tanks & NLR/ALR

Pollutant Potential/Estimated Emissions : Pollutant 1

1. Pollutant Emitted : **VOC**
2. Total Percent Efficiency of Control : %
3. Potential Emissions : lb/hour 9.49 tons/year
4. Synthetically Limited? [ ] Yes [X] No
5. Range of Estimated Fugitive/Other Emissions: to tons/year
6. Emissions Factor : Reference : AP-42
7. Emissions Method Code : 3
8. Calculations of Emissions : See Attachment EU1-1 Total for all general VOC tanks and NLR/ALR
9. Pollutant Potential/Estimated Emissions Comment : Note: the potential hourly emissions is an average value based on 8,760 hours per year.

Emissions Unit Information Section _____

Pollutant Information Section _____

Allowable Emissions _____

1. Basis for Allowable Emissions Code :
2. Future Effective Date of Allowable Emissions :
3. Requested Allowable Emissions and Units :
4. Equivalent Allowable Emissions : lb/hour tons/year
5. Method of Compliance :
6. Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode) :

I. VISIBLE EMISSIONS INFORMATION
(Regulated Emissions Units Only)

Emissions Unit Information Section _____

Visible Emissions Limitation : Visible Emissions Limitation _____

1. Visible Emissions Subtype :
2. Basis for Allowable Opacity :
3. Requested Allowable Opacity : Normal Conditions : % Exceptional Conditions : % Maximum Period of Excess Opacity Allowed : min/hour
4. Method of Compliance :
5. Visible Emissions Comment :

J. CONTINUOUS MONITOR INFORMATION
(Regulated Emissions Units Only)

Emissions Unit Information Section _____

Continuous Monitoring System : Continuous Monitor _____

1. Parameter Code :	2. Pollutant :
3. CMS Requirement :	
4. Monitor Information : Manufacturer : Model Number : Serial Number :	
5. Installation Date :	
6. Performance Specification Test Date :	
7. Continuous Monitor Comment :	

K. PREVENTION OF SIGNIFICANT DETERIORATION (PSD) INCREMENT TRACKING INFORMATION

Emissions Unit Information Section 1

General VOC Storage Tanks & NLR/ALR

PSD Increment Consumption Determination

1. Increment Consuming for Particulate Matter or Sulfur Dioxide?

[ ] The emissions unit is undergoing PSD review as part of this application, or has undergone PSD review previously, for particulate matter or sulfur dioxide. If so, emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after January 6, 1975. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source, and the emissions unit began initial operation after January 6, 1975, but before December 27, 1977. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] For any facility, the emissions unit began (or will begin) initial operation after December 27, 1977. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] None of the above apply. If so, the baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

2. Increment Consuming for Nitrogen Dioxide?

[ ] The emissions unit addressed in this section is undergoing PSD review as part of this application, or has undergone PSD review previously, for nitrogen dioxide. If so, emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after February 8, 1988. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source, and the emissions unit began initial operation after February 8, 1988, but before March 28, 1988. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] For any facility, the emissions unit began (or will begin) initial operation after March 28, 1988. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] None of the above apply. If so, baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

3. Increment Consuming/Expanding Code :		
PM :	SO2 :	NO2 :
4. Baseline Emissions :		
PM :	lb/hour	tons/year
SO2 :	lb/hour	tons/year
NO2 :		tons/year
5. PSD Comment :		
None of the above items apply to this emission unit.		

L. EMISSIONS UNIT SUPPLEMENTAL INFORMATION

Emissions Unit Information Section 1

General VOC Storage Tanks & NLR/ALR

Supplemental Requirements for All Applications

1. Process Flow Diagram :	Waived
2. Fuel Analysis or Specification :	NA
3. Detailed Description of Control Equipment :	NA
4. Description of Stack Sampling Facilities :	NA
5. Compliance Test Report :	NA
6. Procedures for Startup and Shutdown :	NA
7. Operation and Maintenance Plan :	NA
8. Supplemental Information for Construction Permit Application :	NA
9. Other Information Required by Rule or Statue :	EU1-1

Additional Supplemental Requirements for Category I Applications Only

10. Alternative Methods of Operations :	NA
11. Alterntive Modes of Operation (Emissions Trading) :	NA

12. Identification of Additional Applicable Requirements :	NA
13. Compliance Assurance Monitoring Plan :	NA

14. Acid Rain Application (Hard-copy Required) :

NA	Acid Rain Part - Phase II (Form No. 62-210.900(1)(a))
NA	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
NA	New Unit Exemption (Form No. 62-210.900(1)(a)2.)
NA	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)

III. EMISSIONS UNIT INFORMATION

A. TYPE OF EMISSIONS UNIT
(Regulated and Unregulated Emissions Units)

Emissions Unit Information Section 2

Subpart Kb Storage Tanks

Type of Emissions Unit Addressed in This Section

1. Regulated or Unregulated Emissions Unit? Check one :

[X] The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.

[ ] The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.

2. Single Process, Group of Processes, or Fugitive Only? Check one :

[ ] This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).

[X] This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.

[ ] This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only.

Emissions Unit Information Section 2

B. GENERAL EMISSIONS UNIT INFORMATION
(Regulated and Unregulated Emissions Units)

Emissions Unit Description and Status

1. Description of Emissions Unit Addressed in This Section : Subpart Kb Storage Tanks		
2. Emissions Unit Identification Number : [ ] No Corresponding ID [X] Unknown		
3. Emissions Unit Status Code : A	4. Acid Rain Unit? [ ] Yes [X] No	5. Emissions Unit Major Group SIC Code : 51
6. Emissions Unit Comment : The VOC emission source covered under this emission unit consist of 3 storage tanks subject to the NSPS Subpart Kb regulations: Tank nos. 7, 8 and 13. This construction modification application reflects an increased throughput. See attachment EU2-1 for details of the tank.		

Emissions Unit Information Section 2
Subpart Kb Storage Tanks

Emissions Unit Control Equipment 1

1. Description :

VOC controls on storage tank no. 8 will consist of an internal floating roof with a mechanical shoe seal meeting Subpart Kb requirements. Installation of controls on tank no. 8 have not yet been completed, see existing construction permit.

Tank 13 has both primary and secondary seals meeting Subpart Kb requirements.

2. Control Device or Method Code : 99

C. EMISSIONS UNIT DETAIL INFORMATION
(Regulated Emissions Units Only)

Emissions Unit Information Section 2
Subpart Kb Storage Tanks

Emissions Unit Details

1. Initial Startup Date :		
2. Long-term Reserve Shutdown Date :		
3. Package Unit : Manufacturer :		Model Number :
4. Generator Nameplate Rating :	MW	
5. Incinerator Information : Dwell Temperature : Dwell Time : Incinerator Afterburner Temperature :		 Degrees Fahrenheit Seconds Degrees Fahrenheit

Emissions Unit Operating Capacity

1. Maximum Heat Input Rate :	mmBtu/hr	
2. Maximum Incinerator Rate :	lb/hr	tons/day
3. Maximum Process or Throughput Rate :		
4. Maximum Production Rate :		
5. Operating Capacity Comment :		

Emissions Unit Operating Schedule

Requested Maximum Operating Schedule :		
	24 hours/day	7 days/week
	52 weeks/year	8,760 hours/year

D. EMISSIONS UNIT REGULATIONS
(Regulated Emissions Units Only)

Emissions Unit Information Section 2
Subpart Kb Storage Tanks

Rule Applicability Analysis

See attached list.

List of Applicable Regulations

40 CFR 60 Subpart Kb - NSPS for tanks built or modified after July 23, 1984.

E. EMISSION POINT (STACK/VENT) INFORMATION

Emissions Unit Information Section 2

Subpart Kb Storage Tanks

Emission Point Description and Type :

1. Identification of Point on Plot Plan or Flow Diagram :	See plot plan
2. Emission Point Type Code :	3
3. Descriptions of Emission Points Comprising this Emissions Unit : NA	
4. ID Numbers or Descriptions of Emission Units with this Emission Point in Common :	
5. Discharge Type Code :	F
6. Stack Height :	feet
7. Exit Diameter :	feet
8. Exit Temperature :	°F
9. Actual Volumetric Flow Rate :	acfm
10. Percent Water Vapor :	%
11. Maximum Dry Standard Flow Rate :	dscfm
12. Nonstack Emission Point Height :	feet
13. Emission Point UTM Coordinates : Zone : East (km) : North (km) :	
14. Emission Point Comment :	

F. SEGMENT (PROCESS/FUEL) INFORMATION

Emissions Unit Information Section 2

Subpart Kb Storage Tanks

Segment Description and Rate : Segment 1

1. Segment Description (Process/Fuel Type and Associated Operating Method/Mode) : Internal Floating Roof Storage Tank - With Primary and Secondary Seals Gasoline with an average RVP of 11.5 stored	
2. Source Classification Code (SCC) : 4-04-001-79	
3. SCC Units : Thousand Gallons Transferred or Handled	
4. Maximum Hourly Rate :	5. Maximum Annual Rate : 9,072.00
6. Estimated Annual Activity Factor :	
7. Maximum Percent Sulfur :	8. Maximum Percent Ash :
9. Million Btu per SCC Unit :	
10. Segment Comment : This SCC covers Tank No. 13	

F. SEGMENT (PROCESS/FUEL) INFORMATION

Emissions Unit Information Section 2

Subpart Kb Storage Tanks

Segment Description and Rate : Segment 1

1. Segment Description (Process/Fuel Type and Associated Operating Method/Mode) : Internal Floating Roof Storage Tank - With Primary and Secondary Seals Diesel stored	
2. Source Classification Code (SCC) : 4-04-001-99	
3. SCC Units : Thousand Gallons Transferred or Handled	
4. Maximum Hourly Rate :	5. Maximum Annual Rate : 9,072.00
6. Estimated Annual Activity Factor :	
7. Maximum Percent Sulfur :	8. Maximum Percent Ash :
9. Million Btu per SCC Unit :	
10. Segment Comment : This SCC covers Tank No. 13	

F. SEGMENT (PROCESS/FUEL) INFORMATION

Emissions Unit Information Section 2

Subpart Kb Storage Tanks

Segment Description and Rate : Segment 3

1. Segment Description (Process/Fuel Type and Associated Operating Method/Mode) : Fixed roof storage tank - Diesel - Working Loss	
2. Source Classification Code (SCC) : 4-04-001-22	
3. SCC Units : Thousand Gallons Transferred or Handled	
4. Maximum Hourly Rate :	5. Maximum Annual Rate : 70,560.00
6. Estimated Annual Activity Factor :	
7. Maximum Percent Sulfur :	8. Maximum Percent Ash :
9. Million Btu per SCC Unit :	
10. Segment Comment : This SCC covers Tank No. 7	

F. SEGMENT (PROCESS/FUEL) INFORMATION

Emissions Unit Information Section 2

Subpart Kb Storage Tanks

Segment Description and Rate : Segment 4

1. Segment Description (Process/Fuel Type and Associated Operating Method/Mode) : Fixed roof storage tank - Diesel - Standing Loss	
2. Source Classification Code (SCC) : 4-04-001-21	
3. SCC Units : Thousand Gallons Stored	
4. Maximum Hourly Rate :	5. Maximum Annual Rate : 2,253.68
6. Estimated Annual Activity Factor :	
7. Maximum Percent Sulfur :	8. Maximum Percent Ash :
9. Million Btu per SCC Unit :	
10. Segment Comment : This SCC covers tank 7	

G. EMISSIONS UNIT POLLUTANTS
(Regulated and Unregulated Emissions Units)

Emissions Unit Information Section 2
Subpart Kb Storage Tanks

1. Pollutant Emitted	2. Primary Control Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
1 - VOC	099		WP

H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION
(Regulated Emissions Units Only - Emissions Limited Pollutants Only)

Emissions Unit Information Section 2
Subpart Kb Storage Tanks

Pollutant Potential/Estimated Emissions : Pollutant 1

1. Pollutant Emitted : **VOC**
2. Total Percent Efficiency of Control : %
3. Potential Emissions : lb/hour 21.92 tons/year
4. Synthetically Limited? [ ] Yes [X] No
5. Range of Estimated Fugitive/Other Emissions: to tons/year
6. Emissions Factor : Reference : AP-42
7. Emissions Method Code : 3
8. Calculations of Emissions : See Attachment EU2-1
9. Pollutant Potential/Estimated Emissions Comment : Note: the potential hourly emissions is an average value based on 8,760 hours per year.

Emissions Unit Information Section _____

Pollutant Information Section _____

Allowable Emissions _____

1. Basis for Allowable Emissions Code :
2. Future Effective Date of Allowable Emissions :
3. Requested Allowable Emissions and Units :
4. Equivalent Allowable Emissions : lb/hour tons/year
5. Method of Compliance :
6. Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode) :

I. VISIBLE EMISSIONS INFORMATION
(Regulated Emissions Units Only)

Emissions Unit Information Section _____

Visible Emissions Limitation : Visible Emissions Limitation _____

1. Visible Emissions Subtype :
2. Basis for Allowable Opacity :
3. Requested Allowable Opacity : Normal Conditions : % Exceptional Conditions : % Maximum Period of Excess Opacity Allowed : min/hour
4. Method of Compliance :
5. Visible Emissions Comment :

J. CONTINUOUS MONITOR INFORMATION
(Regulated Emissions Units Only)

Emissions Unit Information Section _____

Continuous Monitoring System : Continuous Monitor _____

1. Parameter Code :	2. Pollutant :
3. CMS Requirement :	
4. Monitor Information : Manufacturer : Model Number : Serial Number :	
5. Installation Date :	
6. Performance Specification Test Date :	
7. Continuous Monitor Comment :	

K. PREVENTION OF SIGNIFICANT DETERIORATION (PSD) INCREMENT TRACKING INFORMATION

Emissions Unit Information Section 2

Subpart Kb Storage Tanks

PSD Increment Consumption Determination

1. Increment Consuming for Particulate Matter or Sulfur Dioxide?

[ ] The emissions unit is undergoing PSD review as part of this application, or has undergone PSD review previously, for particulate matter or sulfur dioxide. If so, emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after January 6, 1975. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source, and the emissions unit began initial operation after January 6, 1975, but before December 27, 1977. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] For any facility, the emissions unit began (or will begin) initial operation after December 27, 1977. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] None of the above apply. If so, the baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

2. Increment Consuming for Nitrogen Dioxide?

[ ] The emissions unit addressed in this section is undergoing PSD review as part of this application, or has undergone PSD review previously, for nitrogen dioxide. If so, emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after February 8, 1988. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source, and the emissions unit began initial operation after February 8, 1988, but before March 28, 1988. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] For any facility, the emissions unit began (or will begin) initial operation after March 28, 1988. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] None of the above apply. If so, baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

3. Increment Consuming/Expanding Code :		
PM :	SO2 :	NO2 :
4. Baseline Emissions :		
PM :	lb/hour	tons/year
SO2 :	lb/hour	tons/year
NO2 :		tons/year
5. PSD Comment :		
None of the above items apply to this emission unit.		

L. EMISSIONS UNIT SUPPLEMENTAL INFORMATION

Emissions Unit Information Section 2

Subpart Kb Storage Tanks

Supplemental Requirements for All Applications

1. Process Flow Diagram :	Waived
2. Fuel Analysis or Specification :	NA
3. Detailed Description of Control Equipment :	NA
4. Description of Stack Sampling Facilities :	NA
5. Compliance Test Report :	NA
6. Procedures for Startup and Shutdown :	NA
7. Operation and Maintenance Plan :	NA
8. Supplemental Information for Construction Permit Application :	NA
9. Other Information Required by Rule or Statue :	EU2-1

Additional Supplemental Requirements for Category I Applications Only

10. Alternative Methods of Operations :	NA
11. Alterntive Modes of Operation (Emissions Trading) :	NA

12. Identification of Additional Applicable Requirements :	NA
13. Compliance Assurance Monitoring Plan :	NA

14. Acid Rain Application (Hard-copy Required) :

NA	Acid Rain Part - Phase II (Form No. 62-210.900(1)(a))
NA	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
NA	New Unit Exemption (Form No. 62-210.900(1)(a)2.)
NA	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)

III. EMISSIONS UNIT INFORMATION

A. TYPE OF EMISSIONS UNIT
(Regulated and Unregulated Emissions Units)

Emissions Unit Information Section 3

South Loading Rack - Subpart XX

Type of Emissions Unit Addressed in This Section

1. Regulated or Unregulated Emissions Unit? Check one :

[X] The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.

[ ] The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.

2. Single Process, Group of Processes, or Fugitive Only? Check one :

[ ] This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).

[X] This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.

[ ] This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only.

Emissions Unit Information Section 3

B. GENERAL EMISSIONS UNIT INFORMATION (Regulated and Unregulated Emissions Units)

Emissions Unit Description and Status

1. Description of Emissions Unit Addressed in This Section : South Loading Rack - Subpart XX		
2. Emissions Unit Identification Number : 006 [ ] No Corresponding ID [ ] Unknown		
3. Emissions Unit Status Code : A	4. Acid Rain Unit? [ ] Yes [X] No	5. Emissions Unit Major Group SIC Code : 51
6. Emissions Unit Comment : The VOC emission unit covered under this emission unit consists of the South Loading Rack (SLR) and a flare unit. The modification will result in an increased throughput. See attachment EU3-1 for additional details. Note: The the expansion of the loading rack has not commenced.		

Emissions Unit Information Section 3
South Loading Rack - Subpart XX

Emissions Unit Control Equipment 1

1. Description : VOC controls: an air-assisted vapor flare unit manufactured by Zeeco, Inc. is used. This flare meets the requirements of 40 CFR 60 Subpart XX.
2. Control Device or Method Code : 23

C. EMISSIONS UNIT DETAIL INFORMATION
(Regulated Emissions Units Only)

Emissions Unit Information Section 3
South Loading Rack - Subpart XX

Emissions Unit Details

1. Initial Startup Date :		
2. Long-term Reserve Shutdown Date :		
3. Package Unit : Manufacturer :		Model Number :
4. Generator Nameplate Rating :	MW	
5. Incinerator Information : Dwell Temperature : Dwell Time : Incinerator Afterburner Temperature :		 Degrees Fahrenheit Seconds Degrees Fahrenheit

Emissions Unit Operating Capacity

1. Maximum Heat Input Rate :	mmBtu/hr	
2. Maximum Incinerator Rate :	lb/hr	tons/day
3. Maximum Process or Throughput Rate :		
4. Maximum Production Rate :		
5. Operating Capacity Comment : See attachment EU3-1 for details of the maximum loading rates for each product.		

Emissions Unit Operating Schedule

Requested Maximum Operating Schedule :		
	24 hours/day	7 days/week
	52 weeks/year	8,760 hours/year

D. EMISSIONS UNIT REGULATIONS
(Regulated Emissions Units Only)

Emissions Unit Information Section 3
South Loading Rack - Subpart XX

Rule Applicability Analysis

See attached list.

List of Applicable Regulations

40 CFR 60 Subpart XX - NSPS for gasoline loading racks built or modified after Dec. 17, 1980

E. EMISSION POINT (STACK/VENT) INFORMATION

Emissions Unit Information Section 3

South Loading Rack - Subpart XX

Emission Point Description and Type :

1. Identification of Point on Plot Plan or Flow Diagram :	See plot plan	
2. Emission Point Type Code :	1	
3. Descriptions of Emission Points Comprising this Emissions Unit for VE Tracking : (limit to 100 characters per point)		
4. ID Numbers or Descriptions of Emission Units with this Emission Point in Common :		
5. Discharge Type Code :	V	
6. Stack Height :	36	feet
7. Exit Diameter :	8.0	feet
8. Exit Temperature :	1800	°F
9. Actual Volumetric Flow Rate :	93300	acfm
10. Percent Water Vapor :	9.00	%
11. Maximum Dry Standard Flow Rate :	84903	dscfm
12. Nonstack Emission Point Height :		feet
13. Emission Point UTM Coordinates : Zone : East (km) : North (km) :		
14. Emission Point Comment : See previous applications for exact details of the stack information. Data input is limited by the ELSA program.		

F. SEGMENT (PROCESS/FUEL) INFORMATION

Emissions Unit Information Section 3

South Loading Rack - Subpart XX

Segment Description and Rate : Segment 1

1. Segment Description (Process/Fuel Type and Associated Operating Method/Mode) : Loading Rack with Flare - Gasoline and Diesel Loaded Bulk Terminals - Loading Rack	
2. Source Classification Code (SCC) : 4-04-001-99	
3. SCC Units : Thousand Gallons Transferred or Handled	
4. Maximum Hourly Rate :	5. Maximum Annual Rate : 386,400.00
6. Estimated Annual Activity Factor :	
7. Maximum Percent Sulfur :	8. Maximum Percent Ash :
9. Million Btu per SCC Unit :	
10. Segment Comment : Note: Potential hourly rate is an average based on 8,760 hours per year. This SCC also includes the fugitive emissions from truck loading.	

G. EMISSIONS UNIT POLLUTANTS
(Regulated and Unregulated Emissions Units)

Emissions Unit Information Section 3
South Loading Rack - Subpart XX

1. Pollutant Emitted	2. Primary Control Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
1 - VOC	023		EL

DEP Form No. 62-210.900(1) - Form
Effective : 3-21-96

H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION
(Regulated Emissions Units Only - Emissions Limited Pollutants Only)

Emissions Unit Information Section 3
South Loading Rack - Subpart XX

Pollutant Potential/Estimated Emissions : Pollutant 1

1. Pollutant Emitted : **VOC**
2. Total Percent Efficiency of Control : 98.00 %
3. Potential Emissions : 12.91 lb/hour 56.53 tons/year
4. Synthetically Limited? [X] Yes [ ] No
5. Range of Estimated Fugitive/Other Emissions: to tons/year
6. Emissions Factor : Reference : Subpart XX
7. Emissions Method Code : 0
8. Calculations of Emissions : See Attachment EU8-1
9. Pollutant Potential/Estimated Emissions Comment : Note: the potential hourly emissions is an average value based on 8,760 hours per year.

Emissions Unit Information Section 3
South Loading Rack - Subpart XX

Pollutant Information Section 1

Allowable Emissions 1

1. Basis for Allowable Emissions Code :	RULE		
2. Future Effective Date of Allowable Emissions :			
3. Requested Allowable Emissions and Units :	35.00	mg/l	
4. Equivalent Allowable Emissions :			
	lb/hour	45.99	tons/year
5. Method of Compliance : Stack testing per 40 CFR 60.18			
6. Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode) :			

I. VISIBLE EMISSIONS INFORMATION
(Regulated Emissions Units Only)

Emissions Unit Information Section _____

Visible Emissions Limitation : Visible Emissions Limitation _____

1. Visible Emissions Subtype :
2. Basis for Allowable Opacity :
3. Requested Allowable Opacity : Normal Conditions : % Exceptional Conditions : % Maximum Period of Excess Opacity Allowed : min/hour
4. Method of Compliance :
5. Visible Emissions Comment :

J. CONTINUOUS MONITOR INFORMATION
(Regulated Emissions Units Only)

Emissions Unit Information Section _____

Continuous Monitoring System : Continuous Monitor _____

1. Parameter Code :	2. Pollutant :
3. CMS Requirement :	
4. Monitor Information : Manufacturer : Model Number : Serial Number :	
5. Installation Date :	
6. Performance Specification Test Date :	
7. Continuous Monitor Comment :	

K. PREVENTION OF SIGNIFICANT DETERIORATION (PSD) INCREMENT TRACKING INFORMATION

Emissions Unit Information Section 3

South Loading Rack - Subpart XX

PSD Increment Consumption Determination

1. Increment Consuming for Particulate Matter or Sulfur Dioxide?

[ ] The emissions unit is undergoing PSD review as part of this application, or has undergone PSD review previously, for particulate matter or sulfur dioxide. If so, emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after January 6, 1975. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source, and the emissions unit began initial operation after January 6, 1975, but before December 27, 1977. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] For any facility, the emissions unit began (or will begin) initial operation after December 27, 1977. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] None of the above apply. If so, the baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

2. Increment Consuming for Nitrogen Dioxide?

[ ] The emissions unit addressed in this section is undergoing PSD review as part of this application, or has undergone PSD review previously, for nitrogen dioxide. If so, emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after February 8, 1988. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source, and the emissions unit began initial operation after February 8, 1988, but before March 28, 1988. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] For any facility, the emissions unit began (or will begin) initial operation after March 28, 1988. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] None of the above apply. If so, baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

3. Increment Consuming/Expanding Code :		
PM :	SO2 :	NO2 :
4. Baseline Emissions :		
PM :	lb/hour	tons/year
SO2 :	lb/hour	tons/year
NO2 :		tons/year
5. PSD Comment :		
None of the above items apply to this emission unit.		

L. EMISSIONS UNIT SUPPLEMENTAL INFORMATION

Emissions Unit Information Section 3

South Loading Rack - Subpart XX

Supplemental Requirements for All Applications

1. Process Flow Diagram :	Waived
2. Fuel Analysis or Specification :	NA
3. Detailed Description of Control Equipment :	EU3-1
4. Description of Stack Sampling Facilities :	NA
5. Compliance Test Report :	NA
6. Procedures for Startup and Shutdown :	NA
7. Operation and Maintenance Plan :	NA
8. Supplemental Information for Construction Permit Application :	NA
9. Other Information Required by Rule or Statue :	EU3-2

Additional Supplemental Requirements for Category I Applications Only

10. Alternative Methods of Operations :	NA
11. Alterntive Modes of Operation (Emissions Trading) :	NA

12. Identification of Additional Applicable Requirements :	NA
13. Compliance Assurance Monitoring Plan :	NA

14. Acid Rain Application (Hard-copy Required) :

NA	Acid Rain Part - Phase II (Form No. 62-210.900(1)(a))
NA	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
NA	New Unit Exemption (Form No. 62-210.900(1)(a)2.)
NA	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)

III. EMISSIONS UNIT INFORMATION

A. TYPE OF EMISSIONS UNIT
(Regulated and Unregulated Emissions Units)

Emissions Unit Information Section 4

Subpart K

Type of Emissions Unit Addressed in This Section

1. Regulated or Unregulated Emissions Unit? Check one :

[X] The emissions unit addressed in this Emissions Unit Information Section is a regulated emissions unit.

[ ] The emissions unit addressed in this Emissions Unit Information Section is an unregulated emissions unit.

2. Single Process, Group of Processes, or Fugitive Only? Check one :

[ ] This Emissions Unit Information Section addresses, as a single emissions unit, a single process or production unit, or activity, which produces one or more air pollutants and which has at least one definable emission point (stack or vent).

[X] This Emissions Unit Information Section addresses, as a single emissions unit, a group of process or production units and activities which has at least one definable emission point (stack or vent) but may also produce fugitive emissions.

[ ] This Emissions Unit Information Section addresses, as a single emissions unit, one or more process or production units and activities which produce fugitive emissions only.

Emissions Unit Information Section 4

B. GENERAL EMISSIONS UNIT INFORMATION
(Regulated and Unregulated Emissions Units)

Emissions Unit Description and Status

1. Description of Emissions Unit Addressed in This Section : Subpart K		
2. Emissions Unit Identification Number : [ ] No Corresponding ID [X] Unknown		
3. Emissions Unit Status Code : A	4. Acid Rain Unit? [ ] Yes [X] No	5. Emissions Unit Major Group SIC Code : 51
6. Emissions Unit Comment : The VOC emission sources covered under this emission unit consist of 2 storage tanks subject to the NSPS Subpart K regulations: Tank nos. 17 and 18. This construction modification application reflects an increased throughput. See attachment EU6-1 for details of each tank.		

Emissions Unit Information Section 4
Subpart K

Emissions Unit Control Equipment 1

1. Description : VOC controls on storage tank nos. 17 and 18 consisting of an internal floating roof with primary and secondary seals
2. Control Device or Method Code : 99

C. EMISSIONS UNIT DETAIL INFORMATION
(Regulated Emissions Units Only)

Emissions Unit Information Section 4
Subpart K

Emissions Unit Details

1. Initial Startup Date :		
2. Long-term Reserve Shutdown Date :		
3. Package Unit : Manufacturer :		Model Number :
4. Generator Nameplate Rating :	MW	
5. Incinerator Information : Dwell Temperature : Dwell Time : Incinerator Afterburner Temperature :		 Degrees Fahrenheit Seconds Degrees Fahrenheit

Emissions Unit Operating Capacity

1. Maximum Heat Input Rate :	mmBtu/hr	
2. Maximum Incinerator Rate :	lb/hr	tons/day
3. Maximum Process or Throughput Rate :		
4. Maximum Production Rate :		
5. Operating Capacity Comment :		

Emissions Unit Operating Schedule

Requested Maximum Operating Schedule :	
24 hours/day	7 days/week
52 weeks/year	8,760 hours/year

D. EMISSIONS UNIT REGULATIONS
(Regulated Emissions Units Only)

Emissions Unit Information Section 4
Subpart K

Rule Applicability Analysis

See attached list.

List of Applicable Regulations

40 CFR 60 Subpart K

E. EMISSION POINT (STACK/VENT) INFORMATION

Emissions Unit Information Section _____

Emission Point Description and Type :

1. Identification of Point on Plot Plan or Flow Diagram :	
2. Emission Point Type Code :	
3. Descriptions of Emission Points Comprising this Emissions Unit :	
4. ID Numbers or Descriptions of Emission Units with this Emission Point in Common :	
5. Discharge Type Code :	
6. Stack Height :	feet
7. Exit Diameter :	feet
8. Exit Temperature :	°F
9. Actual Volumetric Flow Rate :	acfm
10. Percent Water Vapor :	%
11. Maximum Dry Standard Flow Rate :	dscfm
12. Nonstack Emission Point Height :	feet
13. Emission Point UTM Coordinates : Zone : East (km) : North (km) :	
14. Emission Point Comment :	

F. SEGMENT (PROCESS/FUEL) INFORMATION

Emissions Unit Information Section 4

Subpart K

Segment Description and Rate : Segment 1

1. Segment Description (Process/Fuel Type and Associated Operating Method/Mode) : Internal Floating Roof Storage Tank - With Primary and Secondary Seals Gasoline with an average RVP of 11.5 stored	
2. Source Classification Code (SCC) : 4-04-001-79	
3. SCC Units : Thousand Gallons Transferred or Handled	
4. Maximum Hourly Rate :	5. Maximum Annual Rate : 168,000.00
6. Estimated Annual Activity Factor :	
7. Maximum Percent Sulfur :	8. Maximum Percent Ash :
9. Million Btu per SCC Unit :	
10. Segment Comment : This SCC covers Tank No. 17 and 18	

G. EMISSIONS UNIT POLLUTANTS
(Regulated and Unregulated Emissions Units)

Emissions Unit Information Section 4
Subpart K

1. Pollutant Emitted	2. Primary Control Device Code	3. Secondary Control Device Code	4. Pollutant Regulatory Code
1 - VOC			WP

H. EMISSIONS UNIT POLLUTANT DETAIL INFORMATION
(Regulated Emissions Units Only - Emissions Limited Pollutants Only)

Emissions Unit Information Section 4
Subpart K

Pollutant Potential/Estimated Emissions : Pollutant 1

1. Pollutant Emitted : **VOC**
2. Total Percent Efficiency of Control : %
3. Potential Emissions : lb/hour 29.08 tons/year
4. Synthetically Limited? [ ] Yes [X] No
5. Range of Estimated Fugitive/Other Emissions: to tons/year
6. Emissions Factor : Reference :
7. Emissions Method Code : 3
8. Calculations of Emissions : See Attachment EU4-1
9. Pollutant Potential/Estimated Emissions Comment : Note: The potential hourly emissions is an average value based on 8,760 hours per year.

Emissions Unit Information Section _____

Pollutant Information Section _____

Allowable Emissions _____

1. Basis for Allowable Emissions Code :
2. Future Effective Date of Allowable Emissions :
3. Requested Allowable Emissions and Units :
4. Equivalent Allowable Emissions : lb/hour tons/year
5. Method of Compliance :
6. Pollutant Allowable Emissions Comment (Desc. of Related Operating Method/Mode) :

I. VISIBLE EMISSIONS INFORMATION
(Regulated Emissions Units Only)

Emissions Unit Information Section _____

Visible Emissions Limitation : Visible Emissions Limitation _____

1. Visible Emissions Subtype :
2. Basis for Allowable Opacity :
3. Requested Allowable Opacity : Normal Conditions : % Exceptional Conditions : % Maximum Period of Excess Opacity Allowed : min/hour
4. Method of Compliance :
5. Visible Emissions Comment :

J. CONTINUOUS MONITOR INFORMATION
(Regulated Emissions Units Only)

Emissions Unit Information Section _____

Continuous Monitoring System : Continuous Monitor _____

1. Parameter Code :	2. Pollutant :
3. CMS Requirement :	
4. Monitor Information : Manufacturer : Model Number : Serial Number :	
5. Installation Date :	
6. Performance Specification Test Date :	
7. Continuous Monitor Comment :	

K. PREVENTION OF SIGNIFICANT DETERIORATION (PSD) INCREMENT TRACKING INFORMATION

Emissions Unit Information Section 4

Subpart K

PSD Increment Consumption Determination

1. Increment Consuming for Particulate Matter or Sulfur Dioxide?

[ ] The emissions unit is undergoing PSD review as part of this application, or has undergone PSD review previously, for particulate matter or sulfur dioxide. If so, emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after January 6, 1975. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source, and the emissions unit began initial operation after January 6, 1975, but before December 27, 1977. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] For any facility, the emissions unit began (or will begin) initial operation after December 27, 1977. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] None of the above apply. If so, the baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

2. Increment Consuming for Nitrogen Dioxide?

[ ] The emissions unit addressed in this section is undergoing PSD review as part of this application, or has undergone PSD review previously, for nitrogen dioxide. If so, emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source pursuant to paragraph (c) of the definition of "major source of air pollution" in Chapter 62-213, F.A.C., and the emissions unit addressed in this section commenced (or will commence) construction after February 8, 1988. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] The facility addressed in this application is classified as an EPA major source, and the emissions unit began initial operation after February 8, 1988, but before March 28, 1988. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] For any facility, the emissions unit began (or will begin) initial operation after March 28, 1988. If so, baseline emissions are zero, and emissions unit consumes increment.

[ ] None of the above apply. If so, baseline emissions of the emissions unit are nonzero. In such case, additional analysis, beyond the scope of this application, is needed to determine whether changes in emissions have occurred (or will occur) after the baseline date that may consume or expand increment.

3. Increment Consuming/Expanding Code :		
PM :	SO2 :	NO2 :
4. Baseline Emissions :		
PM :	lb/hour	tons/year
SO2 :	lb/hour	tons/year
NO2 :		tons/year
5. PSD Comment :		
None of the above items apply to this emission unit.		

L. EMISSIONS UNIT SUPPLEMENTAL INFORMATION

Emissions Unit Information Section 4

Subpart K

Supplemental Requirements for All Applications

1. Process Flow Diagram :	Waived
2. Fuel Analysis or Specification :	NA
3. Detailed Description of Control Equipment :	NA
4. Description of Stack Sampling Facilities :	NA
5. Compliance Test Report :	NA
6. Procedures for Startup and Shutdown :	NA
7. Operation and Maintenance Plan :	NA
8. Supplemental Information for Construction Permit Application :	NA
9. Other Information Required by Rule or Statue :	EU4-1

Additional Supplemental Requirements for Category I Applications Only

10. Alternative Methods of Operations :
11. Alterntive Modes of Operation (Emissions Trading) :

12. Identification of Additional Applicable Requirements :	
13. Compliance Assurance Monitoring Plan :	
14. Acid Rain Application (Hard-copy Required) :	
NA	Acid Rain Part - Phase II (Form No. 62-210.900(1)(a))
NA	Repowering Extension Plan (Form No. 62-210.900(1)(a)1.)
NA	New Unit Exemption (Form No. 62-210.900(1)(a)2.)
NA	Retired Unit Exemption (Form No. 62-210.900(1)(a)3.)

Applicable Regulations

40 CFR 60 Subpart K – NSPS

40 CFR 60 Subpart Kb – NSPS

40 CFR 60 Subpart XX – NSPS

62-296.320(1)

TRANSMONTAIGNE TERMINALING INC.

FACILITY NAME: Cape Canaveral

ANNUAL POTENTIAL TO EMIT SUMMARY SHEET

EQUIPMENT NAME/NO.	EQUIPMENT SPECIFICATIONS				ANNUAL EMISSIONS (ton/yr)									
	DIMENSIONS H X D (ft)	CAPACITY (bbl)	ROOF TYPE	PRODUCT	TANKS 4.09 TOTAL VOC	TOTAL HAPs	Hexane	Benzene	Toluene	Ethyl-benzene	Iso-Octane	Xylene	Cumene	MTBE
1	48 X 120	80,000	CR	Distillate	0.85	0.16	0.0455	0.0565	0.0328	0.0053	na	0.0185	0.0013	na
2	40 X 100	55,832	CR	Asphalt	0.62	0.12	0.0332	0.0412	0.0239	0.0039	na	0.0135	0.0009	na
3	40 X 80	33,607	CR	Asphalt	0.36	0.07	0.0195	0.0242	0.0140	0.0023	na	0.0079	0.0005	na
4	40 X 60	20,000	CR	Asphalt	0.21	0.04	0.0112	0.0139	0.0081	0.0013	na	0.0046	0.0003	na
5	24 X 19	1,200	CR	Asphalt	0.01	0.00	0.0007	0.0009	0.0005	0.0001	na	0.0003	0.0000	na
6	40 X 60	20,000	CR	Asphalt	0.21	0.04	0.0112	0.0139	0.0081	0.0013	na	0.0046	0.0003	na
7	48 X 100	65,269	CR	Distillate	0.69	0.13	0.0370	0.0459	0.0266	0.0043	na	0.0150	0.0010	na
8	40 X 150	121,800	IFR	Gasoline	13.17	0.69	0.2108	0.1186	0.1713	0.0132	0.1054	0.0659	na	na
9	40 X 80	33,740	IFR	Gasoline	4.39	0.23	0.0703	0.0395	0.0571	0.0044	0.0352	0.0220	na	na
10	24 X 30	3,000	CR	Asphalt	0.03	0.01	0.0017	0.0021	0.0012	0.0002	na	0.0007	0.0000	na
11	24 X 30	3,000	CR	Asphalt	0.03	0.01	0.0017	0.0021	0.0012	0.0002	na	0.0007	0.0000	na
12	40 X 40	8,955	CR	Distillate	0.09	0.02	0.0050	0.0062	0.0036	0.0006	na	0.0020	0.0001	na
13	40 X 40	8,048	IFR	Gasoline	2.75	0.14	0.0439	0.0247	0.0357	0.0027	0.0220	0.0137	na	na
14	24 X 21	1,500	CR	Asphalt	0.02	0.00	0.0009	0.0011	0.0006	0.0001	na	0.0003	0.0000	na
15	40 X 100	55,272	EFR	Gasoline	3.72	0.19	0.0595	0.0334	0.0483	0.0037	0.0297	0.0186	na	na
17	42 X 134	98,600	IFR	Gasoline	13.14	0.68	0.2102	0.1183	0.1708	0.0131	0.1051	0.0657	na	na
18	42 X 134	98,100	IFR	Gasoline	13.14	0.68	0.2102	0.1182	0.1708	0.0131	0.1051	0.0657	na	na
23	27 X 8	238	CR	Distillate	0.00	0.00	0.0001	0.0002	0.0001	0.0000	na	0.0001	0.0000	na
24A	20 X 10	190	CR	Distillate	0.00	0.00	0.0001	0.0002	0.0001	0.0000	na	0.0001	0.0000	na
24	16 X 10	238	CR	Additive	-	-	-	-	-	-	-	-	-	-
25	16 X 10	238	CR	PCW	-	-	-	-	-	-	-	-	-	-
26	12 X 5	47	CR	Additive	-	-	-	-	-	-	-	-	-	-
28	4 X 3	11	CR	Additive	-	-	-	-	-	-	-	-	-	-
TOTAL TANK EMISSIONS					53.42	3.21	0.97	0.66	0.77	0.07	0.40	0.32	0.00	-

	PRODUCT	CONTROLS	EMISSION FACTOR (mg/l)	ANNUAL THRUPUT (gal/yr)	ANNUAL EMISSIONS (ton/yr) TOTAL VOC	TOTAL HAPs	Hexane	Benzene	Toluene	Ethyl-benzene	Iso-Octane	Xylene	Cumene	MTBE
Loading Rack	Gasoline	Flare	35.00	315,000,000	46.00	2.39	0.7360	0.4140	0.5980	0.0460	0.3680	0.2300	na	na
	Distillate	Flare	0.093	100,800,000	0.04	0.01	0.0021	0.0026	0.0015	0.0002	na	0.0009	0.0001	na
TOTAL LOADING RACK EMISSIONS					46.04	2.40	0.7381	0.4166	0.5995	0.0462	0.3680	0.2308	0.0001	-

		EMISSION FACTOR (mg/l)	ANNUAL EMISSIONS (ton/yr) Total VOC	Total HAPs	Hexane	Benzene	Toluene	Ethyl-benzene	Iso-Octane	Xylene	Cumene	MTBE
Fugitives	(see page 4)		0.29	0.02	0.0046	0.0026	0.0038	0.0003	0.0023	0.0015	na	na
Cargo Leaks		13.0	17.09	0.89	0.2734	0.1538	0.2221	0.0171	0.1367	0.0854	na	na
TOTAL FUGITIVE EMISSIONS			17.38	0.90	0.2780	0.1564	0.2259	0.0174	0.1390	0.0869	-	-

GRAND TOTAL (ton/yr)									
116.84	6.51	1.9890	1.2339	1.6003	0.1336	0.9095	0.6375	0.0047	-
NOx	5.26	CO	13.15						

NOTES:

1. Hazardous Air Pollutant (HAP) emission factors are as follows:

For Gasoline:

HAP	EF (wt%)
Benzene	0.009
Toluene	0.013
Xylene	0.005
Ethyl Benzene	0.001
IsoOctane	0.008
Hexane	0.016
MTBE	na
TOTAL	0.052

Conventional gasoline does not contain MTBE.

Based on *Hazardous Air Pollutant Emissions from Gasoline Loading Operations at Bulk Gasoline Terminals*, API Publication No. 347, Table 5-2, Pg. 5-3, October 1998

For Distillate: At standard temperature of 68 deg. F.

HAP	EF (wt%)
Benzene	0.0668
Toluene	0.0388
Xylene	0.0219
Ethyl Benzene	0.0063
Cumene	0.0015
Hexane	0.0539
TOTAL	0.1892

Extracted from the *Compilation of Air Emission Factors for Petroleum Distributionand Retail Marketing Facilities*, September 1995

TRANSMONTAIGNE TERMINALING INC.

FACILITY NAME: Cape Canaveral

CALCULATION TABLE 1.

Potential Tank Annual Emission Summary

TANK NO.	ROOF TYPE	CAPACITY (bbls)	CAPACITY (gals)	SERVICE	THRUPUT (gal/yr)	LOSS	EMISSION RATE VOC (lb/yr)	EMISSION RATE VOC (ton/yr)	EMISSION RATE HAPs (lb/yr)	EMISSION RATE HAPs (ton/yr)
8	IFR	121,800	5,115,600	Gasoline	92,326,018	Working	123.75	0.06	6.4350	0.0032
						Breathing	26224.08	13.11	1363.6522	0.6818
9	IFR	33,740	1,417,080	Gasoline	25,575,368	Working	64.44	0.03	3.3509	0.0017
						Breathing	8723.92	4.36	453.6438	0.2268
13	IFR	8,048	338,016	Gasoline	6,100,491	Working	29.55	0.01	1.5366	0.0008
						Breathing	5460.92	2.73	283.9678	0.1420
15	EFR	55,272	2,321,424	Gasoline	41,896,910	Working	79.02	0.04	4.1090	0.0021
						Breathing	7353.99	3.68	382.4075	0.1912
17	IFR	98,600	4,141,200	Gasoline	74,740,110	Working	111.47	0.06	5.7964	0.0029
						Breathing	26166.64	13.08	1360.6653	0.6803
18	IFR	98,100	4,120,200	Gasoline	74,361,103	Working	110.91	0.06	5.7673	0.0029
						Breathing	26166.64	13.08	1360.6653	0.6803
TANK NO.	ROOF TYPE	CAPACITY (bbls)	CAPACITY (gals)	SERVICE	THRUPUT (gal/yr)	LOSS	EMISSION RATE VOC (lb/yr)	EMISSION RATE VOC (ton/yr)	EMISSION RATE HAPs (lb/yr)	EMISSION RATE HAPs (ton/yr)
1	CR	80,000	3,360,000	Distillate	27,541,830	Working	881.11	0.44	45.8177	0.0229
						Breathing	809.02	0.40	42.0690	0.0210
2	CR	55,832	2,344,944	Asphalt	19,221,443	Working	614.93	0.31	31.9764	0.0160
						Breathing	617.67	0.31	32.1188	0.0161
3	CR	33,607	1,411,494	Asphalt	11,569,979	Working	370.14	0.19	19.2473	0.0096
						Breathing	353.06	0.18	18.3591	0.0092
4	CR	20,000	840,000	Asphalt	6,885,458	Working	220.28	0.11	41.6770	0.0208
						Breathing	196.77	0.10	37.2289	0.0186
5	CR	1,200	50,400	Asphalt	413,127	Working	13.22	0.01	2.5012	0.0013
						Breathing	12.27	0.01	2.3215	0.0012
6	CR	20,000	840,000	Asphalt	6,885,458	Working	220.28	0.11	41.6770	0.0208
						Breathing	196.77	0.10	37.2289	0.0186
7	CR	65,269	2,741,298	Distillate	22,470,346	Working	718.87	0.36	136.0102	0.0680
						Breathing	654.10	0.33	123.7557	0.0619
10	CR	3,000	126,000	Asphalt	1,032,819	Working	33.04	0.02	6.2512	0.0031
						Breathing	30.85	0.02	5.8368	0.0029
11	CR	3,000	126,000	Asphalt	1,032,819	Working	33.04	0.02	6.2512	0.0031
						Breathing	30.85	0.02	5.8368	0.0029
12	CR	8,955	376,110	Distillate	3,082,964	Working	98.63	0.05	18.6608	0.0093
						Breathing	86.64	0.04	16.3923	0.0082
14	CR	1,500	63,000	Ashpahlt	516,409	Working	16.52	0.01	3.1256	0.0016
						Breathing	15.02	0.01	2.8418	0.0014
23	CR	238	9,996	Distillate	81,937	Working	2.62	0.00	0.4957	0.0002
						Breathing	2.75	0.00	0.5203	0.0003
24A	CR	190	7,980	Distillate	65,412	Working	2.09	0.00	0.3954	0.0002
						Breathing	2.54	0.00	0.4806	0.0002
TOTAL GASOLINE		415,560	17,453,520		315,000,000		100615.33	50.31	5232.00	2.62
TOTAL ASPHALT/DISTILLATE		292,791	12,297,222		100,800,000		6233.08	3.12	679.08	0.34
TOTAL							**106848.41**	**53.42**	**5911.07**	**2.96**

TANK NO.	ROOF TYPE	CAPACITY (bbls)	CAPACITY (gals)	SERVICE	THRUPUT (gal/yr)	LOSS	EMISSION RATE VOC (lb/yr)	EMISSION RATE VOC (ton/yr)	EMISSION RATE HAPs (lb/yr)	EMISSION RATE HAPs (ton/yr)

NOTES:

1. Tank emissions calculated using US EPA TANKS V. 4.09. See attached TANKS 4.09 Output Report.
2. Conventional gasoline does not contain MTBE. Gasoline HAP emissions based on factors from *Hazardous Air Pollutant Emissions from Gasoline Loading Operations at Bulk Gasoline Terminals*, API Publication No. 347, Table 5-2, Pg. 5-3, October 1998.
3. Distillate HAP emissions based on factors extracted from the *Compilation of Air Emission Factors for Petroleum Distributionand Retail Marketing Facilities*, September 1995.

TRANSMONTAIGNE TERMINALING INC.

FACILITY NAME: Cape Canaveral

CALCULATION TABLE 2.

Potential VOC Emissions from Loading Rack and Associated Control Device

LOADING RACK	PRODUCT	THRUPUT (mgal/yr)	S (-)	MW (lb/mol)	P (psia)	T (R)	Control (%)	LI w/control		EMISSION RATE VOC		EMISSION RATE HAPs	
								(lb/mgal)	(mg/l)	(lb/yr)	(tpy)	(lb/yr)	(tpy)
Loading Rack	Gasoline	315,000	na	na	na	na	na	0.29	35	91,998.56	46.00	4,783.92	2.39
	Distillate	100,800	0.6	130	0.0084	528	95	0.0008	0.093	77.93	0.04	14.74	0.01
TOTAL		415,800								92,076.48	46.04	4,798.67	2.40
Annual VOC Truck Vapor Transit Losses								0.11	13	34,170.89	17.09	1776.89	0.89
Products of Combustion							NOx	0.0334	4.0	13,887.72	6.94		
							CO	0.0835	10.0	34,719.30	17.36		

NOTES:

1. Gasoline and Distillate throughputs based on proposed permit limitations.
2. Gasoline loading rack emission factor based on proposed limitations.
3. Distilltate loading emission factors based on AP-42, Section 5.2.
4. Conventional gasoline does not contain MTBE. Gasoline HAP emissions based on factors from *Hazardous Air Pollutant Emissions from Gasoline Loading Operations at Bulk Gasoline Terminals*, API Publication No. 347, Table 5-2, Pg. 5-3, October 1998.
5. Distillate HAP emissions based on factors extracted from the *Compilation of Air Emission Factors for Petroleum Distributionand Retail Marketing Facilities*, September 1995.
6. Transit Losses based on AP-42, Section 5.2, Table 5.2-5, Return with vapor, Typical transported 13.0 mg/l.
7. NOx and CO emission factors based on manufacturer's guarantee.

TRANSMONTAIGNE TERMINALING INC.

FACILITY NAME: Cape Canaveral

CALCULATION TABLE 3.

Fugitive Emissions Summary

Component Type	Service	No. of Components	Leak Factor		EMISSION RATE			
					VOC		HAPs	
			(kg/hr/comp)	(lb/hr/comp)	(lb/hr)	(tpy)	(lb/hr)	(tpy)
Valves	Light Liquid	149	4.30E-05	9.48E-05	0.01	0.0619	0.0007	3.22E-03
	Gas	197	1.30E-05	2.87E-05	0.01	0.0247	0.0003	1.29E-03
Loading Arm Valves	Light Liquid	5	4.30E-05	9.48E-05	0.00	0.0021	0.0000	1.08E-04
	Gas	11	1.30E-05	2.87E-05	0.00	0.0014	0.0000	7.18E-05
Open-End Lines	Light Liquid	8	1.30E-04	2.87E-04	0.00	0.0100	0.0001	5.22E-04
	Gas	10	1.20E-04	2.65E-04	0.00	0.0116	0.0001	6.03E-04
Fittings (Flanges,	Light Liquid	252	8.00E-06	1.76E-05	0.00	0.0195	0.0002	1.01E-03
Connectors)	Gas	320	4.20E-05	9.26E-05	0.03	0.1298	0.0015	6.75E-03
Pump Seals	Light Liquid	3	5.40E-04	1.19E-03	0.00	0.0156	0.0002	8.14E-04
	Gas	5	6.50E-05	1.43E-04	0.00	0.0031	0.0000	0.00
Other	Light Liquid	4	1.30E-04	2.87E-04	0.00	0.0050	0.0001	0.00
	Gas	5	1.20E-04	2.65E-04	0.00	0.0058	0.0001	3.01E-04
TOTAL		969			0.07	0.29	0.00	0.02

NOTES:

1. Based on *Fugitive Emissions From Equipment Leaks II: Calculation Procedures for Petroleum Industry Facilities* API Publication No. 343, May 1998.

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-1
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Vertical Fixed Roof Tank
Description:	Distillate

Tank Dimensions

Shell Height (ft):	40.00
Diameter (ft):	120.00
Liquid Height (ft):	37.00
Avg. Liquid Height (ft):	18.50
Volume (gallons):	3,360,000.00
Turnovers:	8.20
Net Throughput (gal/yr):	27,541,830.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	0.00
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig):	0.03

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	68.12	62.93	73.30	72.34	0.0084	0.0071	0.0099	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Feb	69.11	63.49	74.73	72.34	0.0087	0.0073	0.0104	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Mar	71.94	65.95	77.92	72.34	0.0095	0.0079	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Apr	74.39	67.88	80.89	72.34	0.0103	0.0084	0.0126	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	May	76.99	70.68	83.30	72.34	0.0112	0.0092	0.0135	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jun	78.67	73.13	84.22	72.34	0.0117	0.0099	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jul	79.14	73.68	84.59	72.34	0.0119	0.0101	0.0141	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Aug	79.03	73.78	84.28	72.34	0.0119	0.0101	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Sep	78.18	73.29	83.08	72.34	0.0116	0.0099	0.0134	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Oct	75.35	70.41	80.28	72.34	0.0106	0.0091	0.0123	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Nov	71.90	66.82	76.98	72.34	0.0095	0.0081	0.0112	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Dec	69.08	64.09	74.07	72.34	0.0087	0.0074	0.0102	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	54.1530	54.9831	70.5503	79.9533	85.6996	75.2445	77.3084	73.8521	64.6193	62.4669	56.9097	53.2809
Vapor Space Volume (cu ft):	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Vented Vapor Saturation Factor:	0.9899	0.9896	0.9886	0.9878	0.9867	0.9860	0.9858	0.9859	0.9862	0.9874	0.9887	0.9896
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380	257,296.4380
Tank Diameter (ft):	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000
Vapor Space Outage (ft):	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500
Tank Shell Height (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Average Liquid Height (ft):	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000
Roof Outage (ft):	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500
Roof Outage (Cone Roof)												
Roof Outage (ft):	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500
Roof Height (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Daily Avg. Liquid Surface Temp. (deg. R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Average Ambient Temp. (deg. F):	59.7000	61.2000	66.6000	71.2000	76.8500	81.1500	82.3000	82.4500	81.0500	75.2000	68.0000	62.1000
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation Factor (Btu/sqft day):	999.0000	1,244.0000	1,582.0000	1,898.0000	1,989.0000	1,831.0000	1,801.0000	1,673.0000	1,497.0000	1,304.0000	1,096.0000	926.0000
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Daily Vapor Temperature Range (deg. R):	20.7392	22.4814	23.9463	26.0265	25.2356	22.1796	21.8208	20.9955	19.5817	19.7430	20.3370	19.9598
Daily Vapor Pressure Range (psia):	0.0028	0.0031	0.0036	0.0042	0.0044	0.0040	0.0040	0.0038	0.0035	0.0033	0.0031	0.0028
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0071	0.0073	0.0079	0.0084	0.0092	0.0099	0.0101	0.0101	0.0099	0.0091	0.0081	0.0074
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0099	0.0104	0.0115	0.0126	0.0135	0.0139	0.0141	0.0139	0.0134	0.0123	0.0112	0.0102
Daily Avg. Liquid Surface Temp. (deg R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Min. Liquid Surface Temp. (deg R):	522.6034	523.1569	525.6206	527.5489	530.3549	532.7987	533.3541	533.4545	532.9556	530.0820	526.4862	523.7562
Daily Max. Liquid Surface Temp. (deg R):	532.9730	534.3976	537.5937	540.5622	542.9727	543.8885	544.2645	543.9522	542.7464	539.9536	536.6547	533.7361
Daily Ambient Temp. Range (deg. R):	22.2000	23.0000	22.8000	23.6000	21.9000	18.7000	18.4000	18.1000	17.3000	18.8000	21.0000	21.6000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9899	0.9896	0.9886	0.9878	0.9867	0.9860	0.9858	0.9859	0.9862	0.9874	0.9887	0.9896
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Space Outage (ft):	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500	22.7500

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	59.9392	61.8614	67.6648	73.0672	79.2363	83.4479	84.6499	84.3752	82.1931	75.2921	67.5866	61.8002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Net Throughput (gal/mo.):	2,295,152.500	2,295,152.500	2,295,152.500	2,295,152.500	2,295,152.500	2,295,152.500	2,295,152.500	2,295,152.500	2,295,152.500	2,295,152.500	2,295,152.500	2,295,152.500
	0	0	0	0	0	0	0	0	0	0	0	0
Annual Turnovers:	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	3,360,000.000	3,360,000.000	3,360,000.000	3,360,000.000	3,360,000.000	3,360,000.000	3,360,000.000	3,360,000.000	3,360,000.000	3,360,000.000	3,360,000.000	3,360,000.000
	0	0	0	0	0	0	0	0	0	0	0	0
Maximum Liquid Height (ft):	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000
Tank Diameter (ft):	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	114.0923	116.8445	138.2151	153.0204	164.9360	158.6925	161.9583	158.2273	146.8124	137.7590	124.4962	115.0811

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	881.11	809.02	1,690.14

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-10
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Vertical Fixed Roof Tank
Description:	Asphalt

Tank Dimensions

Shell Height (ft):	24.00
Diameter (ft):	30.00
Liquid Height (ft):	21.00
Avg. Liquid Height (ft):	10.50
Volume (gallons):	126,000.00
Turnovers:	8.20
Net Throughput (gal/yr):	1,032,819.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	0.00
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig):	0.03

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	68.12	62.93	73.30	72.34	0.0084	0.0071	0.0099	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Feb	69.11	63.49	74.73	72.34	0.0087	0.0073	0.0104	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Mar	71.94	65.95	77.92	72.34	0.0095	0.0079	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Apr	74.39	67.88	80.89	72.34	0.0103	0.0084	0.0126	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	May	76.99	70.68	83.30	72.34	0.0112	0.0092	0.0135	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jun	78.67	73.13	84.22	72.34	0.0117	0.0099	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jul	79.14	73.68	84.59	72.34	0.0119	0.0101	0.0141	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Aug	79.03	73.78	84.28	72.34	0.0119	0.0101	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Sep	78.18	73.29	83.08	72.34	0.0116	0.0099	0.0134	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Oct	75.35	70.41	80.28	72.34	0.0106	0.0091	0.0123	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Nov	71.90	66.82	76.98	72.34	0.0095	0.0081	0.0112	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Dec	69.08	64.09	74.07	72.34	0.0087	0.0074	0.0102	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	2.0631	2.0950	2.6891	3.0486	3.2690	2.8710	2.9500	2.8181	2.4654	2.3822	2.1692	2.0301
Vapor Space Volume (cu ft):	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Vented Vapor Saturation Factor:	0.9939	0.9937	0.9931	0.9925	0.9919	0.9915	0.9914	0.9914	0.9916	0.9923	0.9931	0.9937
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809
Tank Diameter (ft):	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000
Vapor Space Outage (ft):	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125
Tank Shell Height (ft):	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000
Average Liquid Height (ft):	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000
Roof Outage (ft):	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125
Roof Outage (Cone Roof)												
Roof Outage (ft):	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125
Roof Height (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Daily Avg. Liquid Surface Temp. (deg. R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Average Ambient Temp. (deg. F):	59.7000	61.2000	66.6000	71.2000	76.8500	81.1500	82.3000	82.4500	81.0500	75.2000	68.0000	62.1000
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation Factor (Btu/sqft day):	999.0000	1,244.0000	1,582.0000	1,898.0000	1,989.0000	1,831.0000	1,801.0000	1,673.0000	1,497.0000	1,304.0000	1,096.0000	926.0000
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Daily Vapor Temperature Range (deg. R):	20.7392	22.4814	23.9463	26.0265	25.2356	22.1796	21.8208	20.9955	19.5817	19.7430	20.3370	19.9598
Daily Vapor Pressure Range (psia):	0.0028	0.0031	0.0036	0.0042	0.0044	0.0040	0.0040	0.0038	0.0035	0.0033	0.0031	0.0028
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0071	0.0073	0.0079	0.0084	0.0092	0.0099	0.0101	0.0101	0.0099	0.0091	0.0081	0.0074
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0099	0.0104	0.0115	0.0126	0.0135	0.0139	0.0141	0.0139	0.0134	0.0123	0.0112	0.0102
Daily Avg. Liquid Surface Temp. (deg R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Min. Liquid Surface Temp. (deg R):	522.6034	523.1569	525.6206	527.5489	530.3549	532.7987	533.3541	533.4545	532.9556	530.0820	526.4862	523.7562
Daily Max. Liquid Surface Temp. (deg R):	532.9730	534.3976	537.5937	540.5622	542.9727	543.8885	544.2645	543.9522	542.7464	539.9536	536.6547	533.7361
Daily Ambient Temp. Range (deg. R):	22.2000	23.0000	22.8000	23.6000	21.9000	18.7000	18.4000	18.1000	17.3000	18.8000	21.0000	21.6000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9939	0.9937	0.9931	0.9925	0.9919	0.9915	0.9914	0.9914	0.9916	0.9923	0.9931	0.9937
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Space Outage (ft):	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	2.2477	2.3198	2.5374	2.7400	2.9714	3.1293	3.1744	3.1641	3.0822	2.8235	2.5345	2.3175
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Net Throughput (gal/mo.):	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500
Annual Turnovers:	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000
Maximum Liquid Height (ft):	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000
Tank Diameter (ft):	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	4.3108	4.4148	5.2266	5.7886	6.2404	6.0003	6.1244	5.9821	5.5476	5.2057	4.7037	4.3476

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	33.04	30.85	63.89

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-11
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Vertical Fixed Roof Tank
Description:	Asphalt

Tank Dimensions

Shell Height (ft):	24.00
Diameter (ft):	30.00
Liquid Height (ft):	21.00
Avg. Liquid Height (ft):	10.50
Volume (gallons):	126,000.00
Turnovers:	8.20
Net Throughput (gal/yr):	1,032,819.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	0.00
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig):	0.03

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	68.12	62.93	73.30	72.34	0.0084	0.0071	0.0099	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Feb	69.11	63.49	74.73	72.34	0.0087	0.0073	0.0104	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Mar	71.94	65.95	77.92	72.34	0.0095	0.0079	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Apr	74.39	67.88	80.89	72.34	0.0103	0.0084	0.0126	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	May	76.99	70.68	83.30	72.34	0.0112	0.0092	0.0135	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jun	78.67	73.13	84.22	72.34	0.0117	0.0099	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jul	79.14	73.68	84.59	72.34	0.0119	0.0101	0.0141	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Aug	79.03	73.78	84.28	72.34	0.0119	0.0101	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Sep	78.18	73.29	83.08	72.34	0.0116	0.0099	0.0134	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Oct	75.35	70.41	80.28	72.34	0.0106	0.0091	0.0123	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Nov	71.90	66.82	76.98	72.34	0.0095	0.0081	0.0112	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Dec	69.08	64.09	74.07	72.34	0.0087	0.0074	0.0102	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	2.0631	2.0950	2.6891	3.0486	3.2690	2.8710	2.9500	2.8181	2.4654	2.3822	2.1692	2.0301
Vapor Space Volume (cu ft):	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Vented Vapor Saturation Factor:	0.9939	0.9937	0.9931	0.9925	0.9919	0.9915	0.9914	0.9914	0.9916	0.9923	0.9931	0.9937
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809	9,763.4809
Tank Diameter (ft):	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000
Vapor Space Outage (ft):	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125
Tank Shell Height (ft):	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000
Average Liquid Height (ft):	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000
Roof Outage (ft):	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125
Roof Outage (Cone Roof)												
Roof Outage (ft):	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125	0.3125
Roof Height (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000	15.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Daily Avg. Liquid Surface Temp. (deg. R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Average Ambient Temp. (deg. F):	59.7000	61.2000	66.6000	71.2000	76.8500	81.1500	82.3000	82.4500	81.0500	75.2000	68.0000	62.1000
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation Factor (Btu/sqft day):	999.0000	1,244.0000	1,582.0000	1,898.0000	1,989.0000	1,831.0000	1,801.0000	1,673.0000	1,497.0000	1,304.0000	1,096.0000	926.0000
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Daily Vapor Temperature Range (deg. R):	20.7392	22.4814	23.9463	26.0265	25.2356	22.1796	21.8208	20.9955	19.5817	19.7430	20.3370	19.9598
Daily Vapor Pressure Range (psia):	0.0028	0.0031	0.0036	0.0042	0.0044	0.0040	0.0040	0.0038	0.0035	0.0033	0.0031	0.0028
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0071	0.0073	0.0079	0.0084	0.0092	0.0099	0.0101	0.0101	0.0099	0.0091	0.0081	0.0074
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0099	0.0104	0.0115	0.0126	0.0135	0.0139	0.0141	0.0139	0.0134	0.0123	0.0112	0.0102
Daily Avg. Liquid Surface Temp. (deg R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Min. Liquid Surface Temp. (deg R):	522.6034	523.1569	525.6206	527.5489	530.3549	532.7987	533.3541	533.4545	532.9556	530.0820	526.4862	523.7562
Daily Max. Liquid Surface Temp. (deg R):	532.9730	534.3976	537.5937	540.5622	542.9727	543.8885	544.2645	543.9522	542.7464	539.9536	536.6547	533.7361
Daily Ambient Temp. Range (deg. R):	22.2000	23.0000	22.8000	23.6000	21.9000	18.7000	18.4000	18.1000	17.3000	18.8000	21.0000	21.6000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9939	0.9937	0.9931	0.9925	0.9919	0.9915	0.9914	0.9914	0.9916	0.9923	0.9931	0.9937
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Space Outage (ft):	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125	13.8125

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	2.2477	2.3198	2.5374	2.7400	2.9714	3.1293	3.1744	3.1641	3.0822	2.8235	2.5345	2.3175
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Net Throughput (gal/mo.):	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500	86,068.2500
Annual Turnovers:	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000	126,000.0000
Maximum Liquid Height (ft):	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000
Tank Diameter (ft):	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	4.3108	4.4148	5.2266	5.7886	6.2404	6.0003	6.1244	5.9821	5.5476	5.2057	4.7037	4.3476

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	33.04	30.85	63.89

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-12
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Vertical Fixed Roof Tank
Description:	Distillate

Tank Dimensions

Shell Height (ft):	40.00
Diameter (ft):	40.00
Liquid Height (ft):	37.00
Avg. Liquid Height (ft):	18.50
Volume (gallons):	376,110.00
Turnovers:	8.20
Net Throughput (gal/yr):	3,082,964.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	0.00
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig):	0.03

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	68.12	62.93	73.30	72.34	0.0084	0.0071	0.0099	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Feb	69.11	63.49	74.73	72.34	0.0087	0.0073	0.0104	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Mar	71.94	65.95	77.92	72.34	0.0095	0.0079	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Apr	74.39	67.88	80.89	72.34	0.0103	0.0084	0.0126	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	May	76.99	70.68	83.30	72.34	0.0112	0.0092	0.0135	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jun	78.67	73.13	84.22	72.34	0.0117	0.0099	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jul	79.14	73.68	84.59	72.34	0.0119	0.0101	0.0141	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Aug	79.03	73.78	84.28	72.34	0.0119	0.0101	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Sep	78.18	73.29	83.08	72.34	0.0116	0.0099	0.0134	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Oct	75.35	70.41	80.28	72.34	0.0106	0.0091	0.0123	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Nov	71.90	66.82	76.98	72.34	0.0095	0.0081	0.0112	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Dec	69.08	64.09	74.07	72.34	0.0087	0.0074	0.0102	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	5.7987	5.8877	7.5549	8.5621	9.1778	8.0584	8.2795	7.9093	6.9204	6.6896	6.0942	5.7054
Vapor Space Volume (cu ft):	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Vented Vapor Saturation Factor:	0.9903	0.9900	0.9891	0.9882	0.9872	0.9865	0.9863	0.9864	0.9867	0.9878	0.9891	0.9900
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956	27,541.2956
Tank Diameter (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Vapor Space Outage (ft):	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167
Tank Shell Height (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Average Liquid Height (ft):	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000
Roof Outage (ft):	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167
Roof Outage (Cone Roof)												
Roof Outage (ft):	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167	0.4167
Roof Height (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Daily Avg. Liquid Surface Temp. (deg. R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Average Ambient Temp. (deg. F):	59.7000	61.2000	66.6000	71.2000	76.8500	81.1500	82.3000	82.4500	81.0500	75.2000	68.0000	62.1000
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation Factor (Btu/sqft day):	999.0000	1,244.0000	1,582.0000	1,898.0000	1,989.0000	1,831.0000	1,801.0000	1,673.0000	1,497.0000	1,304.0000	1,096.0000	926.0000
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Daily Vapor Temperature Range (deg. R):	20.7392	22.4814	23.9463	26.0265	25.2356	22.1796	21.8208	20.9955	19.5817	19.7430	20.3370	19.9598
Daily Vapor Pressure Range (psia):	0.0028	0.0031	0.0036	0.0042	0.0044	0.0040	0.0040	0.0038	0.0035	0.0033	0.0031	0.0028
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0071	0.0073	0.0079	0.0084	0.0092	0.0099	0.0101	0.0101	0.0099	0.0091	0.0081	0.0074
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0099	0.0104	0.0115	0.0126	0.0135	0.0139	0.0141	0.0139	0.0134	0.0123	0.0112	0.0102
Daily Avg. Liquid Surface Temp. (deg R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Min. Liquid Surface Temp. (deg R):	522.6034	523.1569	525.6206	527.5489	530.3549	532.7987	533.3541	533.4545	532.9556	530.0820	526.4862	523.7562
Daily Max. Liquid Surface Temp. (deg R):	532.9730	534.3976	537.5937	540.5622	542.9727	543.8885	544.2645	543.9522	542.7464	539.9536	536.6547	533.7361
Daily Ambient Temp. Range (deg. R):	22.2000	23.0000	22.8000	23.6000	21.9000	18.7000	18.4000	18.1000	17.3000	18.8000	21.0000	21.6000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9903	0.9900	0.9891	0.9882	0.9872	0.9865	0.9863	0.9864	0.9867	0.9878	0.9891	0.9900
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Space Outage (ft):	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167	21.9167

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	6.7094	6.9246	7.5742	8.1790	8.8695	9.3410	9.4755	9.4448	9.2005	8.4280	7.5655	6.9178
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Net Throughput (gal/mo.):	256,913.6667	256,913.6667	256,913.6667	256,913.6667	256,913.6667	256,913.6667	256,913.6667	256,913.6667	256,913.6667	256,913.6667	256,913.6667	256,913.6667
Annual Turnovers:	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	376,110.0000	376,110.0000	376,110.0000	376,110.0000	376,110.0000	376,110.0000	376,110.0000	376,110.0000	376,110.0000	376,110.0000	376,110.0000	376,110.0000
Maximum Liquid Height (ft):	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000
Tank Diameter (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	12.5082	12.8123	15.1292	16.7411	18.0474	17.3993	17.7550	17.3541	16.1209	15.1176	13.6597	12.6232

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	98.63	86.64	185.27

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-13
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Internal Floating Roof Tank
Description:	Gasoline

Tank Dimensions

Diameter (ft):	40.00
Volume (gallons):	40.00
Turnovers:	152,512.28
Self Supp. Roof? (y/n):	N
No. of Columns:	1.00
Eff. Col. Diam. (ft):	1.10

Paint Characteristics

Internal Shell Condition:	Light Rust
Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Rim-Seal System

Primary Seal:	Vapor-mounted
Secondary Seal:	Rim-mounted

Deck Characteristics

Deck Fitting Category:	Detail
Deck Type:	Bolted
Construction:	Sheet
Deck Seam:	Sheet: 5 Ft Wide
Deck Seam Len. (ft):	251.33

Deck Fitting/Status	Quantity
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	1
Automatic Gauge Float Well/Bolted Cover, Gasketed	1
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	1
Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed	1
Roof Leg or Hanger Well/Adjustable	12
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1
Stub Drain (1-in. Diameter)/	13
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures,(deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Gasoline (RVP 13.5)	Jan	68.12	62.93	73.30	72.34	8.4052	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Feb	69.11	63.49	74.73	72.34	8.5560	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Mar	71.94	65.95	77.92	72.34	8.9991	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Apr	74.39	67.88	80.89	72.34	9.3969	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	May	76.99	70.68	83.30	72.34	9.8358	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Jun	78.67	73.13	84.22	72.34	10.1268	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Jul	79.14	73.68	84.59	72.34	10.2087	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Aug	79.03	73.78	84.28	72.34	10.1900	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Sep	78.18	73.29	83.08	72.34	10.0408	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Oct	75.35	70.41	80.28	72.34	9.5570	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Nov	71.90	66.82	76.98	72.34	8.9932	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Dec	69.08	64.09	74.07	72.34	8.5512	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Rim Seal Losses (lb):	93.8266	96.4204	104.3850	112.0119	121.0249	127.3961	129.2505	128.8253	125.4775	115.2222	104.2762	96.3375
Seal Factor A (lb-mole/ft-yr):	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030
Value of Vapor Pressure Function:	0.2079	0.2137	0.2313	0.2482	0.2682	0.2823	0.2864	0.2855	0.2780	0.2553	0.2311	0.2135
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	8.4052	8.5560	8.9991	9.3969	9.8358	10.1268	10.2087	10.1900	10.0408	9.5570	8.9932	8.5512
Tank Diameter (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Withdrawal Losses (lb):	2.4629	2.4629	2.4629	2.4629	2.4629	2.4629	2.4629	2.4629	2.4629	2.4629	2.4629	2.4629
Number of Columns:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Effective Column Diameter (ft):	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000
Net Throughput (gal/mo.):	508,374.2500	508,374.2500	508,374.2500	508,374.2500	508,374.2500	508,374.2500	508,374.2500	508,374.2500	508,374.2500	508,374.2500	508,374.2500	508,374.2500
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
Average Organic Liquid Density (lb/gal):	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000
Tank Diameter (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Deck Fitting Losses (lb):	236.6990	243.2423	263.3349	282.5754	305.3129	321.3855	326.0639	324.9911	316.5456	290.6741	263.0604	243.0332
Value of Vapor Pressure Function:	0.2079	0.2137	0.2313	0.2482	0.2682	0.2823	0.2864	0.2855	0.2780	0.2553	0.2311	0.2135
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	222.0000	222.0000	222.0000	222.0000	222.0000	222.0000	222.0000	222.0000	222.0000	222.0000	222.0000	222.0000
Deck Seam Losses (lb):	47.7668	49.0873	53.1420	57.0249	61.6134	64.8569	65.8010	65.5845	63.8802	58.6592	53.0866	49.0451
Deck Seam Length (ft):	251.3300	251.3300	251.3300	251.3300	251.3300	251.3300	251.3300	251.3300	251.3300	251.3300	251.3300	251.3300
Deck Seam Loss per Unit Length Factor (lb-mole/ft-yr):	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400
Deck Seam Length Factor(ft/sqft):	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000
Tank Diameter (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000

Deck Fitting/Status	Quantity	Deck Fitting Loss Factors KFa (lb-mole/yr)	KFb (lb-mole/(yr mph^n))	m	Losses (lb.)
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	1	1.60	0.00	0.00	24.6454
Automatic Gauge Float Well/Bolted Cover, Gasketed	1	2.80	0.00	0.00	43.1294
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	1	33.00	0.00	0.00	508.3108
Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed	1	56.00	0.00	0.00	862.5880
Roof Leg or Hanger Well/Adjustable	12	7.90	0.00	0.00	1,460.2383
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1	12.00	0.00	0.00	184.8403
Stub Drain (1-in. Diameter)/	13	1.20	0.00	0.00	240.2924
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1	6.20	1.20	0.94	95.5008

Total Losses (lb):	380.7554	391.2129	423.3248	454.0751	490.4142	516.1013	523.5783	521.8638	508.3662	467.0184	422.8861	390.8786

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)				
Components	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Gasoline (RVP 13.5)	1,354.45	29.55	3,416.92	689.55	5,490.48

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-14
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Vertical Fixed Roof Tank
Description:	Asphalt

Tank Dimensions

Shell Height (ft):	24.00
Diameter (ft):	21.00
Liquid Height (ft):	21.00
Avg. Liquid Height (ft):	10.50
Volume (gallons):	63,000.00
Turnovers:	8.20
Net Throughput (gal/yr):	516,409.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	0.00
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig):	0.03

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	68.12	62.93	73.30	72.34	0.0084	0.0071	0.0099	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Feb	69.11	63.49	74.73	72.34	0.0087	0.0073	0.0104	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Mar	71.94	65.95	77.92	72.34	0.0095	0.0079	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Apr	74.39	67.88	80.89	72.34	0.0103	0.0084	0.0126	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	May	76.99	70.68	83.30	72.34	0.0112	0.0092	0.0135	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jun	78.67	73.13	84.22	72.34	0.0117	0.0099	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jul	79.14	73.68	84.59	72.34	0.0119	0.0101	0.0141	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Aug	79.03	73.78	84.28	72.34	0.0119	0.0101	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Sep	78.18	73.29	83.08	72.34	0.0116	0.0099	0.0134	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Oct	75.35	70.41	80.28	72.34	0.0106	0.0091	0.0123	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Nov	71.90	66.82	76.98	72.34	0.0095	0.0081	0.0112	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Dec	69.08	64.09	74.07	72.34	0.0087	0.0074	0.0102	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	1.0041	1.0196	1.3088	1.4838	1.5910	1.3973	1.4358	1.3716	1.1999	1.1594	1.0557	0.9880
Vapor Space Volume (cu ft):	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Vented Vapor Saturation Factor:	0.9939	0.9937	0.9931	0.9926	0.9920	0.9915	0.9914	0.9914	0.9917	0.9924	0.9931	0.9937
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343	4,751.6343
Tank Diameter (ft):	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000
Vapor Space Outage (ft):	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188
Tank Shell Height (ft):	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000
Average Liquid Height (ft):	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000
Roof Outage (ft):	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188
Roof Outage (Cone Roof)												
Roof Outage (ft):	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188	0.2188
Roof Height (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000
Vapor Density												
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Daily Avg. Liquid Surface Temp. (deg. R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Average Ambient Temp. (deg. F):	59.7000	61.2000	66.6000	71.2000	76.8500	81.1500	82.3000	82.4500	81.0500	75.2000	68.0000	62.1000
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation Factor (Btu/sqft day):	999.0000	1,244.0000	1,582.0000	1,898.0000	1,989.0000	1,831.0000	1,801.0000	1,673.0000	1,497.0000	1,304.0000	1,096.0000	926.0000
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Daily Vapor Temperature Range (deg. R):	20.7392	22.4814	23.9463	26.0265	25.2356	22.1796	21.8208	20.9955	19.5817	19.7430	20.3370	19.9598
Daily Vapor Pressure Range (psia):	0.0028	0.0031	0.0036	0.0042	0.0044	0.0040	0.0040	0.0038	0.0035	0.0033	0.0031	0.0028
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0071	0.0073	0.0079	0.0084	0.0092	0.0099	0.0101	0.0101	0.0099	0.0091	0.0081	0.0074
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0099	0.0104	0.0115	0.0126	0.0135	0.0139	0.0141	0.0139	0.0134	0.0123	0.0112	0.0102
Daily Avg. Liquid Surface Temp. (deg R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Min. Liquid Surface Temp. (deg R):	522.6034	523.1569	525.6206	527.5489	530.3549	532.7987	533.3541	533.4545	532.9556	530.0820	526.4862	523.7562
Daily Max. Liquid Surface Temp. (deg R):	532.9730	534.3976	537.5937	540.5622	542.9727	543.8885	544.2645	543.9522	542.7464	539.9536	536.6547	533.7361
Daily Ambient Temp. Range (deg. R):	22.2000	23.0000	22.8000	23.6000	21.9000	18.7000	18.4000	18.1000	17.3000	18.8000	21.0000	21.6000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9939	0.9937	0.9931	0.9926	0.9920	0.9915	0.9914	0.9914	0.9917	0.9924	0.9931	0.9937
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Space Outage (ft):	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188	13.7188

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	1.1239	1.1599	1.2687	1.3700	1.4857	1.5646	1.5872	1.5820	1.5411	1.4117	1.2672	1.1588
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Net Throughput (gal/mo.):	43,034.0833	43,034.0833	43,034.0833	43,034.0833	43,034.0833	43,034.0833	43,034.0833	43,034.0833	43,034.0833	43,034.0833	43,034.0833	43,034.0833
Annual Turnovers:	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	63,000.0000	63,000.0000	63,000.0000	63,000.0000	63,000.0000	63,000.0000	63,000.0000	63,000.0000	63,000.0000	63,000.0000	63,000.0000	63,000.0000
Maximum Liquid Height (ft):	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000
Tank Diameter (ft):	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	2.1279	2.1795	2.5775	2.8538	3.0767	2.9620	3.0230	2.9536	2.7410	2.5711	2.3230	2.1468

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	16.52	15.02	31.54

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-15
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	External Floating Roof Tank
Description:	Gasoline

Tank Dimensions

Diameter (ft):	100.00
Volume (gallons):	2,321,424.00
Turnovers:	18.05

Paint Characteristics

Internal Shell Condition:	Light Rust
Shell Color/Shade:	White/White
Shell Condition:	Good

Roof Characteristics

Type:	Pontoon
Fitting Category:	Detail

Tank Construction and Rim-Seal System

Construction:	Welded
Primary Seal:	Mechanical Shoe
Secondary Seal:	Rim-mounted

Deck Fitting/Status	Quantity
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	1
Automatic Gauge Float Well/Bolted Cover, Gasketed	1
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	1
Gauge-Hatch/Sample Well (8-in. Diam.)/Weighted Mech. Actuation, Gask.	1
Roof Leg (3-in. Diameter)/Adjustable, Pontoon Area, Gasketed	17
Rim Vent (6-in. Diameter)/Weighted Mech. Actuation, Gask.	1

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Gasoline (RVP 13.5)	Jan	68.12	62.93	73.30	72.34	8.4052	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Feb	69.11	63.49	74.73	72.34	8.5560	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Mar	71.94	65.95	77.92	72.34	8.9991	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Apr	74.39	67.88	80.89	72.34	9.3969	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	May	76.99	70.68	83.30	72.34	9.8358	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Jun	78.67	73.13	84.22	72.34	10.1268	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Jul	79.14	73.68	84.59	72.34	10.2087	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Aug	79.03	73.78	84.28	72.34	10.1900	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Sep	78.18	73.29	83.08	72.34	10.0408	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Oct	75.35	70.41	80.28	72.34	9.5570	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Nov	71.90	66.82	76.98	72.34	8.9932	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Dec	69.08	64.09	74.07	72.34	8.5512	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Rim Seal Losses (lb):	447.8090	486.4847	540.9041	554.9680	566.6168	550.1193	522.8772	509.4454	519.0207	528.9746	483.4623	437.8976
Seal Factor A (lb-mole/ft-yr):	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000
Average Wind Speed (mph):	9.0000	9.6000	9.9000	9.4000	8.8000	8.0000	7.4000	7.2000	7.6000	8.6000	8.7000	8.5000
Seal-related Wind Speed Exponent:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Value of Vapor Pressure Function:	0.2079	0.2137	0.2313	0.2482	0.2682	0.2823	0.2864	0.2855	0.2780	0.2553	0.2311	0.2135
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	8.4052	8.5560	8.9991	9.3969	9.8358	10.1268	10.2087	10.1900	10.0408	9.5570	8.9932	8.5512
Tank Diameter (ft):	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Withdrawal Losses (lb):	6.5848	6.5848	6.5848	6.5848	6.5848	6.5848	6.5848	6.5848	6.5848	6.5848	6.5848	6.5848
Net Throughput (gal/mo.):	3,491,409.166	3,491,409.166	3,491,409.166	3,491,409.166	3,491,409.166	3,491,409.166	3,491,409.166	3,491,409.166	3,491,409.166	3,491,409.166	3,491,409.166	3,491,409.166
	0	0	0	0	0	0	0	0	0	0	0	0
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
Average Organic Liquid Density (lb/gal):	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000
Tank Diameter (ft):	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000
Roof Fitting Losses (lb):	84.1217	87.1767	94.7701	100.9918	108.1996	112.5918	113.2263	112.5175	110.2473	102.7185	93.0932	85.7602
Value of Vapor Pressure Function:	0.2079	0.2137	0.2313	0.2482	0.2682	0.2823	0.2864	0.2855	0.2780	0.2553	0.2311	0.2135
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	78.8977	79.5636	79.8943	79.3423	78.6744	77.7738	77.0899	76.8602	77.3187	78.4504	78.5625	78.3381
Average Wind Speed (mph):	9.0000	9.6000	9.9000	9.4000	8.8000	8.0000	7.4000	7.2000	7.6000	8.6000	8.7000	8.5000

Roof Fitting/Status	Quantity	Roof Fitting Loss Factors KFa (lb-mole/yr)	KFb (lb-mole/(yr mph^n))	m	Losses (lb.)
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	1	1.60	0.00	0.00	24.6454
Automatic Gauge Float Well/Bolted Cover, Gasketed	1	2.80	0.00	0.00	43.1294
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1	6.20	1.20	0.94	194.0779
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	1	33.00	0.00	0.00	508.3108
Gauge-Hatch/Sample Well (8-in. Diam.)/Weighted Mech. Actuation, Gask.	1	0.47	0.02	0.97	8.9729
Roof Leg (3-in. Diameter)/Adjustable, Pontoon Area, Gasketed	17	1.30	0.08	0.65	407.0102
Rim Vent (6-in. Diameter)/Weighted Mech. Actuation, Gask.	1	0.71	0.10	1.00	20.0802

Total Losses (lb):	538.5155	580.2462	642.2590	662.5446	681.4012	669.2959	642.6883	628.5477	635.8528	638.2778	583.1402	530.2426

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)				
Components	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Gasoline (RVP 13.5)	6,148.58	79.02	1,205.41	0.00	7,433.01

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-17
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Internal Floating Roof Tank
Description:	Gasoline

Tank Dimensions

Diameter (ft):	134.00
Volume (gallons):	4,141,200.00
Turnovers:	18.05
Self Supp. Roof? (y/n):	N
No. of Columns:	8.00
Eff. Col. Diam. (ft):	1.00

Paint Characteristics

Internal Shell Condition:	Light Rust
Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Rim-Seal System

Primary Seal:	Vapor-mounted
Secondary Seal:	Rim-mounted

Deck Characteristics

Deck Fitting Category:	Detail
Deck Type:	Bolted
Construction:	Sheet
Deck Seam:	Sheet: 5 Ft Wide
Deck Seam Len. (ft):	2,820.52

Deck Fitting/Status	Quantity
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	1
Automatic Gauge Float Well/Bolted Cover, Gasketed	1
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	8
Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed	1
Roof Leg or Hanger Well/Adjustable	49
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1
Stub Drain (1-in. Diameter)/	144
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Gasoline (RVP 13.5)	Jan	68.12	62.93	73.30	72.34	8.4052	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Feb	69.11	63.49	74.73	72.34	8.5560	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Mar	71.94	65.95	77.92	72.34	8.9991	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Apr	74.39	67.88	80.89	72.34	9.3969	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	May	76.99	70.68	83.30	72.34	9.8358	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Jun	78.67	73.13	84.22	72.34	10.1268	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Jul	79.14	73.68	84.59	72.34	10.2087	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Aug	79.03	73.78	84.28	72.34	10.1900	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Sep	78.18	73.29	83.08	72.34	10.0408	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Oct	75.35	70.41	80.28	72.34	9.5570	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Nov	71.90	66.82	76.98	72.34	8.9932	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Dec	69.08	64.09	74.07	72.34	8.5512	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Rim Seal Losses (lb):	314.3193	323.0083	349.6898	375.2398	405.4336	426.7768	432.9893	431.5647	420.3498	385.9943	349.3252	322.7305
Seal Factor A (lb-mole/ft-yr):	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030
Value of Vapor Pressure Function:	0.2079	0.2137	0.2313	0.2482	0.2682	0.2823	0.2864	0.2855	0.2780	0.2553	0.2311	0.2135
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	8.4052	8.5560	8.9991	9.3969	9.8358	10.1268	10.2087	10.1900	10.0408	9.5570	8.9932	8.5512
Tank Diameter (ft):	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Withdrawal Losses (lb):	9.2895	9.2895	9.2895	9.2895	9.2895	9.2895	9.2895	9.2895	9.2895	9.2895	9.2895	9.2895
Number of Columns:	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000
Effective Column Diameter (ft):	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Net Throughput (gal/mo.):	6,228,342.500	6,228,342.500	6,228,342.500	6,228,342.500	6,228,342.500	6,228,342.500	6,228,342.500	6,228,342.500	6,228,342.500	6,228,342.500	6,228,342.500	6,228,342.500
	0	0	0	0	0	0	0	0	0	0	0	0
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
Average Organic Liquid Density (lb/gal):	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000
Tank Diameter (ft):	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000
Deck Fitting Losses (lb):	962.2562	988.8568	1,070.5394	1,148.7583	1,241.1933	1,306.5334	1,325.5524	1,321.1911	1,286.8577	1,181.6820	1,069.4233	988.0065
Value of Vapor Pressure Function:	0.2079	0.2137	0.2313	0.2482	0.2682	0.2823	0.2864	0.2855	0.2780	0.2553	0.2311	0.2135
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000
Deck Seam Losses (lb):	536.0573	550.8760	596.3801	639.9546	691.4486	727.8485	738.4437	736.0141	716.8875	658.2959	595.7583	550.4024
Deck Seam Length (ft):	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200
Deck Seam Loss per Unit Length Factor (lb-mole/ft-yr):	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400
Deck Seam Length Factor(ft/sqft):	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000
Tank Diameter (ft):	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000

Deck Fitting/Status	Quantity	Deck Fitting Loss Factors KFa (lb-mole/yr)	KFb (lb-mole/(yr mph^n))	m	Losses (lb.)
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	1	1.60	0.00	0.00	24.6454
Automatic Gauge Float Well/Bolted Cover, Gasketed	1	2.80	0.00	0.00	43.1294
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	8	33.00	0.00	0.00	4,066.4865
Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed	1	56.00	0.00	0.00	862.5880
Roof Leg or Hanger Well/Adjustable	49	7.90	0.00	0.00	5,962.6399
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1	12.00	0.00	0.00	184.8403
Stub Drain (1-in. Diameter)/	144	1.20	0.00	0.00	2,661.7003
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1	6.20	1.20	0.94	95.5008

Total Losses (lb):	1,821.9223	1,872.0306	2,025.8988	2,173.2422	2,347.3651	2,470.4482	2,506.2750	2,498.0594	2,433.3845	2,235.2617	2,023.7963	1,870.4289

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)				
Components	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Gasoline (RVP 13.5)	4,537.42	111.47	13,890.85	7,738.37	26,278.11

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-18
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Internal Floating Roof Tank
Description:	Gasoline

Tank Dimensions

Diameter (ft):	134.00
Volume (gallons):	4,120,200.00
Turnovers:	18.05
Self Supp. Roof? (y/n):	N
No. of Columns:	8.00
Eff. Col. Diam. (ft):	1.00

Paint Characteristics

Internal Shell Condition:	Light Rust
Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Rim-Seal System

Primary Seal:	Vapor-mounted
Secondary Seal:	Rim-mounted

Deck Characteristics

Deck Fitting Category:	Detail
Deck Type:	Bolted
Construction:	Sheet
Deck Seam:	Sheet: 5 Ft Wide
Deck Seam Len. (ft):	2,820.52

Deck Fitting/Status	Quantity
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	1
Automatic Gauge Float Well/Bolted Cover, Gasketed	1
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	8
Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed	1
Roof Leg or Hanger Well/Adjustable	49
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1
Stub Drain (1-in. Diameter)/	144
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Gasoline (RVP 13.5)	Jan	68.12	62.93	73.30	72.34	8.4052	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Feb	69.11	63.49	74.73	72.34	8.5560	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Mar	71.94	65.95	77.92	72.34	8.9991	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Apr	74.39	67.88	80.89	72.34	9.3969	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	May	76.99	70.68	83.30	72.34	9.8358	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Jun	78.67	73.13	84.22	72.34	10.1268	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Jul	79.14	73.68	84.59	72.34	10.2087	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Aug	79.03	73.78	84.28	72.34	10.1900	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Sep	78.18	73.29	83.08	72.34	10.0408	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Oct	75.35	70.41	80.28	72.34	9.5570	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Nov	71.90	66.82	76.98	72.34	8.9932	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Dec	69.08	64.09	74.07	72.34	8.5512	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Rim Seal Losses (lb):	314.3193	323.0083	349.6898	375.2398	405.4336	426.7768	432.9893	431.5647	420.3498	385.9943	349.3252	322.7305
Seal Factor A (lb-mole/ft-yr):	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000	2.2000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030	0.0030
Value of Vapor Pressure Function:	0.2079	0.2137	0.2313	0.2482	0.2682	0.2823	0.2864	0.2855	0.2780	0.2553	0.2311	0.2135
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	8.4052	8.5560	8.9991	9.3969	9.8358	10.1268	10.2087	10.1900	10.0408	9.5570	8.9932	8.5512
Tank Diameter (ft):	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Withdrawal Losses (lb):	9.2424	9.2424	9.2424	9.2424	9.2424	9.2424	9.2424	9.2424	9.2424	9.2424	9.2424	9.2424
Number of Columns:	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000
Effective Column Diameter (ft):	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Net Throughput (gal/mo.):	6,196,758.583	6,196,758.583	6,196,758.583	6,196,758.583	6,196,758.583	6,196,758.583	6,196,758.583	6,196,758.583	6,196,758.583	6,196,758.583	6,196,758.583	6,196,758.583
	0	0	0	0	0	0	0	0	0	0	0	0
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
Average Organic Liquid Density (lb/gal):	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000
Tank Diameter (ft):	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000
Deck Fitting Losses (lb):	962.2562	988.8568	1,070.5394	1,148.7583	1,241.1933	1,306.5334	1,325.5524	1,321.1911	1,286.8577	1,181.6820	1,069.4233	988.0065
Value of Vapor Pressure Function:	0.2079	0.2137	0.2313	0.2482	0.2682	0.2823	0.2864	0.2855	0.2780	0.2553	0.2311	0.2135
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000	902.5000
Deck Seam Losses (lb):	536.0573	550.8760	596.3801	639.9546	691.4486	727.8485	738.4437	736.0141	716.8875	658.2959	595.7583	550.4024
Deck Seam Length (ft):	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200	2,820.5200
Deck Seam Loss per Unit Length Factor (lb-mole/ft-yr):	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400
Deck Seam Length Factor(ft/sqft):	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000
Tank Diameter (ft):	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000	134.0000
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000

Deck Fitting/Status	Quantity	Deck Fitting Loss Factors KFa (lb-mole/yr)	KFb (lb-mole/(yr mph^n))	m	Losses (lb.)
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	1	1.60	0.00	0.00	24.6454
Automatic Gauge Float Well/Bolted Cover, Gasketed	1	2.80	0.00	0.00	43.1294
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	8	33.00	0.00	0.00	4,066.4865
Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed	1	56.00	0.00	0.00	862.5880
Roof Leg or Hanger Well/Adjustable	49	7.90	0.00	0.00	5,962.6399
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1	12.00	0.00	0.00	184.8403
Stub Drain (1-in. Diameter)/	144	1.20	0.00	0.00	2,661.7003
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1	6.20	1.20	0.94	95.5008

Total Losses (lb):	1,821.8752	1,871.9835	2,025.8516	2,173.1951	2,347.3180	2,470.4011	2,506.2279	2,498.0123	2,433.3374	2,235.2146	2,023.7492	1,870.3818

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)				
Components	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Gasoline (RVP 13.5)	4,537.42	110.91	13,890.85	7,738.37	26,277.55

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-2
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Vertical Fixed Roof Tank
Description:	Asphalt

Tank Dimensions

Shell Height (ft):	40.00
Diameter (ft):	100.00
Liquid Height (ft):	37.00
Avg. Liquid Height (ft):	18.50
Volume (gallons):	2,344,944.00
Turnovers:	8.20
Net Throughput (gal/yr):	19,221,443.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	0.00
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	0.00
Pressure Settings (psig):	0.00

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	68.12	62.93	73.30	72.34	0.0084	0.0071	0.0099	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Feb	69.11	63.49	74.73	72.34	0.0087	0.0073	0.0104	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Mar	71.94	65.95	77.92	72.34	0.0095	0.0079	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Apr	74.39	67.88	80.89	72.34	0.0103	0.0084	0.0126	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	May	76.99	70.68	83.30	72.34	0.0112	0.0092	0.0135	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jun	78.67	73.13	84.22	72.34	0.0117	0.0099	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jul	79.14	73.68	84.59	72.34	0.0119	0.0101	0.0141	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Aug	79.03	73.78	84.28	72.34	0.0119	0.0101	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Sep	78.18	73.29	83.08	72.34	0.0116	0.0099	0.0134	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Oct	75.35	70.41	80.28	72.34	0.0106	0.0091	0.0123	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Nov	71.90	66.82	76.98	72.34	0.0095	0.0081	0.0112	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Dec	69.08	64.09	74.07	72.34	0.0087	0.0074	0.0102	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	41.5493	41.8214	53.3452	60.0050	64.5285	57.4190	59.1050	56.7087	50.0284	48.2833	43.7986	41.0729
Vapor Space Volume (cu ft):	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Space Expansion Factor:	0.0395	0.0427	0.0453	0.0490	0.0473	0.0415	0.0408	0.0392	0.0366	0.0371	0.0385	0.0379
Vented Vapor Saturation Factor:	0.9900	0.9897	0.9887	0.9879	0.9868	0.9862	0.9860	0.9860	0.9864	0.9875	0.9888	0.9897
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358	177,041.8358
Tank Diameter (ft):	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000
Vapor Space Outage (ft):	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417
Tank Shell Height (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Average Liquid Height (ft):	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000
Roof Outage (ft):	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417
Roof Outage (Cone Roof)												
Roof Outage (ft):	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417
Roof Height (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Daily Avg. Liquid Surface Temp. (deg. R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Average Ambient Temp. (deg. F):	59.7000	61.2000	66.6000	71.2000	76.8500	81.1500	82.3000	82.4500	81.0500	75.2000	68.0000	62.1000
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation Factor (Btu/sqft day):	999.0000	1,244.0000	1,582.0000	1,898.0000	1,989.0000	1,831.0000	1,801.0000	1,673.0000	1,497.0000	1,304.0000	1,096.0000	926.0000
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0395	0.0427	0.0453	0.0490	0.0473	0.0415	0.0408	0.0392	0.0366	0.0371	0.0385	0.0379
Daily Vapor Temperature Range (deg. R):	20.7392	22.4814	23.9463	26.0265	25.2356	22.1796	21.8208	20.9955	19.5817	19.7430	20.3370	19.9598
Daily Vapor Pressure Range (psia):	0.0028	0.0031	0.0036	0.0042	0.0044	0.0040	0.0040	0.0038	0.0035	0.0033	0.0031	0.0028
Breather Vent Press. Setting Range(psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0071	0.0073	0.0079	0.0084	0.0092	0.0099	0.0101	0.0101	0.0099	0.0091	0.0081	0.0074
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0099	0.0104	0.0115	0.0126	0.0135	0.0139	0.0141	0.0139	0.0134	0.0123	0.0112	0.0102
Daily Avg. Liquid Surface Temp. (deg R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Min. Liquid Surface Temp. (deg R):	522.6034	523.1569	525.6206	527.5489	530.3549	532.7987	533.3541	533.4545	532.9556	530.0820	526.4862	523.7562
Daily Max. Liquid Surface Temp. (deg R):	532.9730	534.3976	537.5937	540.5622	542.9727	543.8885	544.2645	543.9522	542.7464	539.9536	536.6547	533.7361
Daily Ambient Temp. Range (deg. R):	22.2000	23.0000	22.8000	23.6000	21.9000	18.7000	18.4000	18.1000	17.3000	18.8000	21.0000	21.6000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9900	0.9897	0.9887	0.9879	0.9868	0.9862	0.9860	0.9860	0.9864	0.9875	0.9888	0.9897
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Space Outage (ft):	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417	22.5417

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	41.8316	43.1731	47.2233	50.9936	55.2990	58.2383	59.0771	58.8855	57.3625	52.5464	47.1687	43.1304
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Net Throughput (gal/mo.):	1,601,786.916	1,601,786.916	1,601,786.916	1,601,786.916	1,601,786.916	1,601,786.916	1,601,786.916	1,601,786.916	1,601,786.916	1,601,786.916	1,601,786.916	1,601,786.916
	0	0	0	0	0	0	0	0	0	0	0	0
Annual Turnovers:	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	2,344,944.000	2,344,944.000	2,344,944.000	2,344,944.000	2,344,944.000	2,344,944.000	2,344,944.000	2,344,944.000	2,344,944.000	2,344,944.000	2,344,944.000	2,344,944.000
	0	0	0	0	0	0	0	0	0	0	0	0
Maximum Liquid Height (ft):	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000
Tank Diameter (ft):	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	83.3808	84.9945	100.5685	110.9985	119.8275	115.6573	118.1822	115.5942	107.3909	100.8296	90.9673	84.2033

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	614.93	617.67	1,232.59

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-23
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Horizontal Tank
Description:	Distillate

Tank Dimensions

Shell Length (ft):	27.00
Diameter (ft):	8.00
Volume (gallons):	9,996.00
Turnovers:	8.20
Net Throughput (gal/yr):	81,937.00
Is Tank Heated (y/n):	N
Is Tank Underground (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition:	Good

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig):	0.03

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	68.12	62.93	73.30	72.34	0.0084	0.0071	0.0099	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Feb	69.11	63.49	74.73	72.34	0.0087	0.0073	0.0104	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Mar	71.94	65.95	77.92	72.34	0.0095	0.0079	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Apr	74.39	67.88	80.89	72.34	0.0103	0.0084	0.0126	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	May	76.99	70.68	83.30	72.34	0.0112	0.0092	0.0135	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jun	78.67	73.13	84.22	72.34	0.0117	0.0099	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jul	79.14	73.68	84.59	72.34	0.0119	0.0101	0.0141	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Aug	79.03	73.78	84.28	72.34	0.0119	0.0101	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Sep	78.18	73.29	83.08	72.34	0.0116	0.0099	0.0134	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Oct	75.35	70.41	80.28	72.34	0.0106	0.0091	0.0123	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Nov	71.90	66.82	76.98	72.34	0.0095	0.0081	0.0112	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Dec	69.08	64.09	74.07	72.34	0.0087	0.0074	0.0102	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	0.1835	0.1863	0.2393	0.2714	0.2911	0.2557	0.2628	0.2510	0.2196	0.2121	0.1930	0.1806
Vapor Space Volume (cu ft):	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Vented Vapor Saturation Factor:	0.9982	0.9982	0.9980	0.9978	0.9976	0.9975	0.9975	0.9975	0.9976	0.9978	0.9980	0.9982
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382	864.4382
Tank Diameter (ft):	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000
Effective Diameter (ft):	16.5879	16.5879	16.5879	16.5879	16.5879	16.5879	16.5879	16.5879	16.5879	16.5879	16.5879	16.5879
Vapor Space Outage (ft):	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000
Tank Shell Length (ft):	27.0000	27.0000	27.0000	27.0000	27.0000	27.0000	27.0000	27.0000	27.0000	27.0000	27.0000	27.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Daily Avg. Liquid Surface Temp. (deg. R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Average Ambient Temp. (deg. F):	59.7000	61.2000	66.6000	71.2000	76.8500	81.1500	82.3000	82.4500	81.0500	75.2000	68.0000	62.1000
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation Factor (Btu/sqft day):	999.0000	1,244.0000	1,582.0000	1,898.0000	1,989.0000	1,831.0000	1,801.0000	1,673.0000	1,497.0000	1,304.0000	1,096.0000	926.0000
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Daily Vapor Temperature Range (deg. R):	20.7392	22.4814	23.9463	26.0265	25.2356	22.1796	21.8208	20.9955	19.5817	19.7430	20.3370	19.9598
Daily Vapor Pressure Range (psia):	0.0028	0.0031	0.0036	0.0042	0.0044	0.0040	0.0040	0.0038	0.0035	0.0033	0.0031	0.0028
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0071	0.0073	0.0079	0.0084	0.0092	0.0099	0.0101	0.0101	0.0099	0.0091	0.0081	0.0074
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0099	0.0104	0.0115	0.0126	0.0135	0.0139	0.0141	0.0139	0.0134	0.0123	0.0112	0.0102
Daily Avg. Liquid Surface Temp. (deg R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Min. Liquid Surface Temp. (deg R):	522.6034	523.1569	525.6206	527.5489	530.3549	532.7987	533.3541	533.4545	532.9556	530.0820	526.4862	523.7562
Daily Max. Liquid Surface Temp. (deg R):	532.9730	534.3976	537.5937	540.5622	542.9727	543.8885	544.2645	543.9522	542.7464	539.9536	536.6547	533.7361
Daily Ambient Temp. Range (deg. R):	22.2000	23.0000	22.8000	23.6000	21.9000	18.7000	18.4000	18.1000	17.3000	18.8000	21.0000	21.6000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9982	0.9982	0.9980	0.9978	0.9976	0.9975	0.9975	0.9975	0.9976	0.9978	0.9980	0.9982
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Space Outage (ft):	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000
Working Losses (lb):	0.1783	0.1840	0.2013	0.2174	0.2357	0.2483	0.2518	0.2510	0.2445	0.2240	0.2011	0.1839
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Net Throughput (gal/mo.):	6,828.0833	6,828.0833	6,828.0833	6,828.0833	6,828.0833	6,828.0833	6,828.0833	6,828.0833	6,828.0833	6,828.0833	6,828.0833	6,828.0833
Annual Turnovers:	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tank Diameter (ft):	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	0.3618	0.3704	0.4406	0.4887	0.5268	0.5040	0.5146	0.5021	0.4641	0.4361	0.3941	0.3644

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	2.62	2.75	5.37

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-24A
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Horizontal Tank
Description:	Distillate

Tank Dimensions

Shell Length (ft):	16.00
Diameter (ft):	10.00
Volume (gallons):	7,980.00
Turnovers:	8.20
Net Throughput (gal/yr):	65,412.00
Is Tank Heated (y/n):	N
Is Tank Underground (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition:	Good

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig):	0.03

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures,(deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	68.12	62.93	73.30	72.34	0.0084	0.0071	0.0099	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Feb	69.11	63.49	74.73	72.34	0.0087	0.0073	0.0104	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Mar	71.94	65.95	77.92	72.34	0.0095	0.0079	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Apr	74.39	67.88	80.89	72.34	0.0103	0.0084	0.0126	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	May	76.99	70.68	83.30	72.34	0.0112	0.0092	0.0135	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jun	78.67	73.13	84.22	72.34	0.0117	0.0099	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jul	79.14	73.68	84.59	72.34	0.0119	0.0101	0.0141	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Aug	79.03	73.78	84.28	72.34	0.0119	0.0101	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Sep	78.18	73.29	83.08	72.34	0.0116	0.0099	0.0134	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Oct	75.35	70.41	80.28	72.34	0.0106	0.0091	0.0123	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Nov	71.90	66.82	76.98	72.34	0.0095	0.0081	0.0112	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Dec	69.08	64.09	74.07	72.34	0.0087	0.0074	0.0102	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	0.1698	0.1724	0.2214	0.2511	0.2694	0.2367	0.2432	0.2323	0.2032	0.1963	0.1786	0.1671
Vapor Space Volume (cu ft):	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Vented Vapor Saturation Factor:	0.9978	0.9977	0.9975	0.9973	0.9971	0.9969	0.9969	0.9969	0.9969	0.9972	0.9975	0.9977
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058	800.4058
Tank Diameter (ft):	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000
Effective Diameter (ft):	14.2766	14.2766	14.2766	14.2766	14.2766	14.2766	14.2766	14.2766	14.2766	14.2766	14.2766	14.2766
Vapor Space Outage (ft):	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000
Tank Shell Length (ft):	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Daily Avg. Liquid Surface Temp. (deg. R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Average Ambient Temp. (deg. F):	59.7000	61.2000	66.6000	71.2000	76.8500	81.1500	82.3000	82.4500	81.0500	75.2000	68.0000	62.1000
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation Factor (Btu/sqft day):	999.0000	1,244.0000	1,582.0000	1,898.0000	1,989.0000	1,831.0000	1,801.0000	1,673.0000	1,497.0000	1,304.0000	1,096.0000	926.0000
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Daily Vapor Temperature Range (deg. R):	20.7392	22.4814	23.9463	26.0265	25.2356	22.1796	21.8208	20.9955	19.5817	19.7430	20.3370	19.9598
Daily Vapor Pressure Range (psia):	0.0028	0.0031	0.0036	0.0042	0.0044	0.0040	0.0040	0.0038	0.0035	0.0033	0.0031	0.0028
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0071	0.0073	0.0079	0.0084	0.0092	0.0099	0.0101	0.0101	0.0099	0.0091	0.0081	0.0074
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0099	0.0104	0.0115	0.0126	0.0135	0.0139	0.0141	0.0139	0.0134	0.0123	0.0112	0.0102
Daily Avg. Liquid Surface Temp. (deg R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Min. Liquid Surface Temp. (deg R):	522.6034	523.1569	525.6206	527.5489	530.3549	532.7987	533.3541	533.4545	532.9556	530.0820	526.4862	523.7562
Daily Max. Liquid Surface Temp. (deg R):	532.9730	534.3976	537.5937	540.5622	542.9727	543.8885	544.2645	543.9522	542.7464	539.9536	536.6547	533.7361
Daily Ambient Temp. Range (deg. R):	22.2000	23.0000	22.8000	23.6000	21.9000	18.7000	18.4000	18.1000	17.3000	18.8000	21.0000	21.6000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9978	0.9977	0.9975	0.9973	0.9971	0.9969	0.9969	0.9969	0.9969	0.9972	0.9975	0.9977
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Space Outage (ft):	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000
Working Losses (lb):	0.1424	0.1469	0.1607	0.1735	0.1882	0.1982	0.2010	0.2004	0.1952	0.1788	0.1605	0.1468
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Net Throughput (gal/mo.):	5,451.0000	5,451.0000	5,451.0000	5,451.0000	5,451.0000	5,451.0000	5,451.0000	5,451.0000	5,451.0000	5,451.0000	5,451.0000	5,451.0000
Annual Turnovers:	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tank Diameter (ft):	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	0.3122	0.3194	0.3821	0.4247	0.4576	0.4348	0.4442	0.4327	0.3984	0.3751	0.3391	0.3139

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	2.09	2.54	4.63

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-3
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Vertical Fixed Roof Tank
Description:	Aspahlt

Tank Dimensions

Shell Height (ft):	40.00
Diameter (ft):	80.00
Liquid Height (ft):	37.00
Avg. Liquid Height (ft):	18.50
Volume (gallons):	1,411,494.00
Turnovers:	8.20
Net Throughput (gal/yr):	11,569,979.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	0.00
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig):	0.03

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	68.12	62.93	73.30	72.34	0.0084	0.0071	0.0099	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Feb	69.11	63.49	74.73	72.34	0.0087	0.0073	0.0104	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Mar	71.94	65.95	77.92	72.34	0.0095	0.0079	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Apr	74.39	67.88	80.89	72.34	0.0103	0.0084	0.0126	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	May	76.99	70.68	83.30	72.34	0.0112	0.0092	0.0135	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jun	78.67	73.13	84.22	72.34	0.0117	0.0099	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jul	79.14	73.68	84.59	72.34	0.0119	0.0101	0.0141	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Aug	79.03	73.78	84.28	72.34	0.0119	0.0101	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Sep	78.18	73.29	83.08	72.34	0.0116	0.0099	0.0134	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Oct	75.35	70.41	80.28	72.34	0.0106	0.0091	0.0123	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Nov	71.90	66.82	76.98	72.34	0.0095	0.0081	0.0112	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Dec	69.08	64.09	74.07	72.34	0.0087	0.0074	0.0102	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	23.6316	23.9939	30.7878	34.8918	37.4002	32.8379	33.7387	32.2303	28.2008	27.2609	24.8351	23.2511
Vapor Space Volume (cu ft):	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Vented Vapor Saturation Factor:	0.9901	0.9898	0.9889	0.9880	0.9870	0.9863	0.9861	0.9861	0.9865	0.9876	0.9889	0.9898
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774	112,259.5774
Tank Diameter (ft):	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000
Vapor Space Outage (ft):	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333
Tank Shell Height (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Average Liquid Height (ft):	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000
Roof Outage (ft):	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333
Roof Outage (Cone Roof)												
Roof Outage (ft):	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333
Roof Height (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Daily Avg. Liquid Surface Temp. (deg. R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Average Ambient Temp. (deg. F):	59.7000	61.2000	66.6000	71.2000	76.8500	81.1500	82.3000	82.4500	81.0500	75.2000	68.0000	62.1000
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation Factor (Btu/sqft day):	999.0000	1,244.0000	1,582.0000	1,898.0000	1,989.0000	1,831.0000	1,801.0000	1,673.0000	1,497.0000	1,304.0000	1,096.0000	926.0000
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Daily Vapor Temperature Range (deg. R):	20.7392	22.4814	23.9463	26.0265	25.2356	22.1796	21.8208	20.9955	19.5817	19.7430	20.3370	19.9598
Daily Vapor Pressure Range (psia):	0.0028	0.0031	0.0036	0.0042	0.0044	0.0040	0.0040	0.0038	0.0035	0.0033	0.0031	0.0028
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0071	0.0073	0.0079	0.0084	0.0092	0.0099	0.0101	0.0101	0.0099	0.0091	0.0081	0.0074
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0099	0.0104	0.0115	0.0126	0.0135	0.0139	0.0141	0.0139	0.0134	0.0123	0.0112	0.0102
Daily Avg. Liquid Surface Temp. (deg R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Min. Liquid Surface Temp. (deg R):	522.6034	523.1569	525.6206	527.5489	530.3549	532.7987	533.3541	533.4545	532.9556	530.0820	526.4862	523.7562
Daily Max. Liquid Surface Temp. (deg R):	532.9730	534.3976	537.5937	540.5622	542.9727	543.8885	544.2645	543.9522	542.7464	539.9536	536.6547	533.7361
Daily Ambient Temp. Range (deg. R):	22.2000	23.0000	22.8000	23.6000	21.9000	18.7000	18.4000	18.1000	17.3000	18.8000	21.0000	21.6000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9901	0.9898	0.9889	0.9880	0.9870	0.9863	0.9861	0.9861	0.9865	0.9876	0.9889	0.9898
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Space Outage (ft):	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333	22.3333

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	25.1797	25.9872	28.4251	30.6946	33.2862	35.0554	35.5604	35.4450	34.5283	31.6293	28.3923	25.9615
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Net Throughput (gal/mo.):	964,164.9167	964,164.9167	964,164.9167	964,164.9167	964,164.9167	964,164.9167	964,164.9167	964,164.9167	964,164.9167	964,164.9167	964,164.9167	964,164.9167
Annual Turnovers:	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	1,411,494.000	1,411,494.000	1,411,494.000	1,411,494.000	1,411,494.000	1,411,494.000	1,411,494.000	1,411,494.000	1,411,494.000	1,411,494.000	1,411,494.000	1,411,494.000
	0	0	0	0	0	0	0	0	0	0	0	0
Maximum Liquid Height (ft):	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000
Tank Diameter (ft):	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	48.8113	49.9811	59.2130	65.5864	70.6864	67.8934	69.2991	67.6753	62.7291	58.8902	53.2274	49.2126

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	370.14	353.06	723.21

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-4
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Vertical Fixed Roof Tank
Description:	Asphalt

Tank Dimensions

Shell Height (ft):	40.00
Diameter (ft):	60.00
Liquid Height (ft):	37.00
Avg. Liquid Height (ft):	18.50
Volume (gallons):	840,000.00
Turnovers:	8.20
Net Throughput (gal/yr):	6,885,458.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	0.00
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig):	0.03

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures,(deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	68.12	62.93	73.30	72.34	0.0084	0.0071	0.0099	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Feb	69.11	63.49	74.73	72.34	0.0087	0.0073	0.0104	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Mar	71.94	65.95	77.92	72.34	0.0095	0.0079	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Apr	74.39	67.88	80.89	72.34	0.0103	0.0084	0.0126	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	May	76.99	70.68	83.30	72.34	0.0112	0.0092	0.0135	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jun	78.67	73.13	84.22	72.34	0.0117	0.0099	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jul	79.14	73.68	84.59	72.34	0.0119	0.0101	0.0141	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Aug	79.03	73.78	84.28	72.34	0.0119	0.0101	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Sep	78.18	73.29	83.08	72.34	0.0116	0.0099	0.0134	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Oct	75.35	70.41	80.28	72.34	0.0106	0.0091	0.0123	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Nov	71.90	66.82	76.98	72.34	0.0095	0.0081	0.0112	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Dec	69.08	64.09	74.07	72.34	0.0087	0.0074	0.0102	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	13.1700	13.3720	17.1584	19.4457	20.8439	18.3014	18.8034	17.9628	15.7170	15.1930	13.8409	12.9580
Vapor Space Volume (cu ft):	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Vented Vapor Saturation Factor:	0.9902	0.9899	0.9890	0.9881	0.9871	0.9864	0.9862	0.9863	0.9866	0.9877	0.9890	0.9899
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636
Tank Diameter (ft):	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000
Vapor Space Outage (ft):	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250
Tank Shell Height (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Average Liquid Height (ft):	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000
Roof Outage (ft):	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250
Roof Outage (Cone Roof)												
Roof Outage (ft):	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250
Roof Height (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Daily Avg. Liquid Surface Temp. (deg. R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Average Ambient Temp. (deg. F):	59.7000	61.2000	66.6000	71.2000	76.8500	81.1500	82.3000	82.4500	81.0500	75.2000	68.0000	62.1000
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation Factor (Btu/sqft day):	999.0000	1,244.0000	1,582.0000	1,898.0000	1,989.0000	1,831.0000	1,801.0000	1,673.0000	1,497.0000	1,304.0000	1,096.0000	926.0000
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Daily Vapor Temperature Range (deg. R):	20.7392	22.4814	23.9463	26.0265	25.2356	22.1796	21.8208	20.9955	19.5817	19.7430	20.3370	19.9598
Daily Vapor Pressure Range (psia):	0.0028	0.0031	0.0036	0.0042	0.0044	0.0040	0.0040	0.0038	0.0035	0.0033	0.0031	0.0028
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0071	0.0073	0.0079	0.0084	0.0092	0.0099	0.0101	0.0101	0.0099	0.0091	0.0081	0.0074
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0099	0.0104	0.0115	0.0126	0.0135	0.0139	0.0141	0.0139	0.0134	0.0123	0.0112	0.0102
Daily Avg. Liquid Surface Temp. (deg R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Min. Liquid Surface Temp. (deg R):	522.6034	523.1569	525.6206	527.5489	530.3549	532.7987	533.3541	533.4545	532.9556	530.0820	526.4862	523.7562
Daily Max. Liquid Surface Temp. (deg R):	532.9730	534.3976	537.5937	540.5622	542.9727	543.8885	544.2645	543.9522	542.7464	539.9536	536.6547	533.7361
Daily Ambient Temp. Range (deg. R):	22.2000	23.0000	22.8000	23.6000	21.9000	18.7000	18.4000	18.1000	17.3000	18.8000	21.0000	21.6000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9902	0.9899	0.9890	0.9881	0.9871	0.9864	0.9862	0.9863	0.9866	0.9877	0.9890	0.9899
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Space Outage (ft):	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	14.9848	15.4654	16.9162	18.2668	19.8091	20.8620	21.1625	21.0938	20.5483	18.8230	16.8966	15.4501
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Net Throughput (gal/mo.):	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667
Annual Turnovers:	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000
Maximum Liquid Height (ft):	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000
Tank Diameter (ft):	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	28.1548	28.8373	34.0746	37.7125	40.6530	39.1633	39.9659	39.0566	36.2652	34.0160	30.7375	28.4080

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	220.28	196.77	417.04

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-5
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Vertical Fixed Roof Tank
Description:	Distillate

Tank Dimensions

Shell Height (ft):	24.00
Diameter (ft):	19.00
Liquid Height (ft):	21.00
Avg. Liquid Height (ft):	10.50
Volume (gallons):	50,400.00
Turnovers:	8.20
Net Throughput (gal/yr):	413,127.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	0.00
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig):	0.03

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures,(deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	68.12	62.93	73.30	72.34	0.0084	0.0071	0.0099	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Feb	69.11	63.49	74.73	72.34	0.0087	0.0073	0.0104	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Mar	71.94	65.95	77.92	72.34	0.0095	0.0079	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Apr	74.39	67.88	80.89	72.34	0.0103	0.0084	0.0126	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	May	76.99	70.68	83.30	72.34	0.0112	0.0092	0.0135	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jun	78.67	73.13	84.22	72.34	0.0117	0.0099	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jul	79.14	73.68	84.59	72.34	0.0119	0.0101	0.0141	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Aug	79.03	73.78	84.28	72.34	0.0119	0.0101	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Sep	78.18	73.29	83.08	72.34	0.0116	0.0099	0.0134	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Oct	75.35	70.41	80.28	72.34	0.0106	0.0091	0.0123	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Nov	71.90	66.82	76.98	72.34	0.0095	0.0081	0.0112	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Dec	69.08	64.09	74.07	72.34	0.0087	0.0074	0.0102	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	0.8207	0.8334	1.0698	1.2128	1.3005	1.1421	1.1735	1.1211	0.9808	0.9477	0.8629	0.8076
Vapor Space Volume (cu ft):	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Vented Vapor Saturation Factor:	0.9939	0.9937	0.9931	0.9926	0.9920	0.9915	0.9914	0.9915	0.9917	0.9924	0.9931	0.9937
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530	3,883.7530
Tank Diameter (ft):	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000
Vapor Space Outage (ft):	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979
Tank Shell Height (ft):	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000
Average Liquid Height (ft):	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000	10.5000
Roof Outage (ft):	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979
Roof Outage (Cone Roof)												
Roof Outage (ft):	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979	0.1979
Roof Height (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	9.5000	9.5000	9.5000	9.5000	9.5000	9.5000	9.5000	9.5000	9.5000	9.5000	9.5000	9.5000
Vapor Density												
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Daily Avg. Liquid Surface Temp. (deg. R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Average Ambient Temp. (deg. F):	59.7000	61.2000	66.6000	71.2000	76.8500	81.1500	82.3000	82.4500	81.0500	75.2000	68.0000	62.1000
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation Factor (Btu/sqft day):	999.0000	1,244.0000	1,582.0000	1,898.0000	1,989.0000	1,831.0000	1,801.0000	1,673.0000	1,497.0000	1,304.0000	1,096.0000	926.0000
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Daily Vapor Temperature Range (deg. R):	20.7392	22.4814	23.9463	26.0265	25.2356	22.1796	21.8208	20.9955	19.5817	19.7430	20.3370	19.9598
Daily Vapor Pressure Range (psia):	0.0028	0.0031	0.0036	0.0042	0.0044	0.0040	0.0040	0.0038	0.0035	0.0033	0.0031	0.0028
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0071	0.0073	0.0079	0.0084	0.0092	0.0099	0.0101	0.0101	0.0099	0.0091	0.0081	0.0074
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0099	0.0104	0.0115	0.0126	0.0135	0.0139	0.0141	0.0139	0.0134	0.0123	0.0112	0.0102
Daily Avg. Liquid Surface Temp. (deg R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Min. Liquid Surface Temp. (deg R):	522.6034	523.1569	525.6206	527.5489	530.3549	532.7987	533.3541	533.4545	532.9556	530.0820	526.4862	523.7562
Daily Max. Liquid Surface Temp. (deg R):	532.9730	534.3976	537.5937	540.5622	542.9727	543.8885	544.2645	543.9522	542.7464	539.9536	536.6547	533.7361
Daily Ambient Temp. Range (deg. R):	22.2000	23.0000	22.8000	23.6000	21.9000	18.7000	18.4000	18.1000	17.3000	18.8000	21.0000	21.6000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9939	0.9937	0.9931	0.9926	0.9920	0.9915	0.9914	0.9915	0.9917	0.9924	0.9931	0.9937
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Space Outage (ft):	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979	13.6979

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	0.8991	0.9279	1.0150	1.0960	1.1885	1.2517	1.2697	1.2656	1.2329	1.1294	1.0138	0.9270
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Net Throughput (gal/mo.):	34,427.2500	34,427.2500	34,427.2500	34,427.2500	34,427.2500	34,427.2500	34,427.2500	34,427.2500	34,427.2500	34,427.2500	34,427.2500	34,427.2500
Annual Turnovers:	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	50,400.0000	50,400.0000	50,400.0000	50,400.0000	50,400.0000	50,400.0000	50,400.0000	50,400.0000	50,400.0000	50,400.0000	50,400.0000	50,400.0000
Maximum Liquid Height (ft):	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000	21.0000
Tank Diameter (ft):	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000	19.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	1.7198	1.7613	2.0847	2.3088	2.4890	2.3938	2.4433	2.3867	2.2137	2.0770	1.8767	1.7346

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	13.22	12.27	25.49

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-6
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Vertical Fixed Roof Tank
Description:	Asphalt

Tank Dimensions

Shell Height (ft):	40.00
Diameter (ft):	60.00
Liquid Height (ft):	37.00
Avg. Liquid Height (ft):	18.50
Volume (gallons):	840,000.00
Turnovers:	8.20
Net Throughput (gal/yr):	6,885,458.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	0.00
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig):	0.03

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	68.12	62.93	73.30	72.34	0.0084	0.0071	0.0099	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Feb	69.11	63.49	74.73	72.34	0.0087	0.0073	0.0104	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Mar	71.94	65.95	77.92	72.34	0.0095	0.0079	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Apr	74.39	67.88	80.89	72.34	0.0103	0.0084	0.0126	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	May	76.99	70.68	83.30	72.34	0.0112	0.0092	0.0135	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jun	78.67	73.13	84.22	72.34	0.0117	0.0099	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jul	79.14	73.68	84.59	72.34	0.0119	0.0101	0.0141	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Aug	79.03	73.78	84.28	72.34	0.0119	0.0101	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Sep	78.18	73.29	83.08	72.34	0.0116	0.0099	0.0134	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Oct	75.35	70.41	80.28	72.34	0.0106	0.0091	0.0123	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Nov	71.90	66.82	76.98	72.34	0.0095	0.0081	0.0112	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Dec	69.08	64.09	74.07	72.34	0.0087	0.0074	0.0102	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	13.1700	13.3720	17.1584	19.4457	20.8439	18.3014	18.8034	17.9628	15.7170	15.1930	13.8409	12.9580
Vapor Space Volume (cu ft):	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Vented Vapor Saturation Factor:	0.9902	0.9899	0.9890	0.9881	0.9871	0.9864	0.9862	0.9863	0.9866	0.9877	0.9890	0.9899
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636	62,556.9636
Tank Diameter (ft):	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000
Vapor Space Outage (ft):	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250
Tank Shell Height (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Average Liquid Height (ft):	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000	18.5000
Roof Outage (ft):	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250
Roof Outage (Cone Roof)												
Roof Outage (ft):	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250	0.6250
Roof Height (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Daily Avg. Liquid Surface Temp. (deg. R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Average Ambient Temp. (deg. F):	59.7000	61.2000	66.6000	71.2000	76.8500	81.1500	82.3000	82.4500	81.0500	75.2000	68.0000	62.1000
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation Factor (Btu/sqft day):	999.0000	1,244.0000	1,582.0000	1,898.0000	1,989.0000	1,831.0000	1,801.0000	1,673.0000	1,497.0000	1,304.0000	1,096.0000	926.0000
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Daily Vapor Temperature Range (deg. R):	20.7392	22.4814	23.9463	26.0265	25.2356	22.1796	21.8208	20.9955	19.5817	19.7430	20.3370	19.9598
Daily Vapor Pressure Range (psia):	0.0028	0.0031	0.0036	0.0042	0.0044	0.0040	0.0040	0.0038	0.0035	0.0033	0.0031	0.0028
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0071	0.0073	0.0079	0.0084	0.0092	0.0099	0.0101	0.0101	0.0099	0.0091	0.0081	0.0074
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0099	0.0104	0.0115	0.0126	0.0135	0.0139	0.0141	0.0139	0.0134	0.0123	0.0112	0.0102
Daily Avg. Liquid Surface Temp. (deg R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Min. Liquid Surface Temp. (deg R):	522.6034	523.1569	525.6206	527.5489	530.3549	532.7987	533.3541	533.4545	532.9556	530.0820	526.4862	523.7562
Daily Max. Liquid Surface Temp. (deg R):	532.9730	534.3976	537.5937	540.5622	542.9727	543.8885	544.2645	543.9522	542.7464	539.9536	536.6547	533.7361
Daily Ambient Temp. Range (deg. R):	22.2000	23.0000	22.8000	23.6000	21.9000	18.7000	18.4000	18.1000	17.3000	18.8000	21.0000	21.6000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9902	0.9899	0.9890	0.9881	0.9871	0.9864	0.9862	0.9863	0.9866	0.9877	0.9890	0.9899
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Space Outage (ft):	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250	22.1250

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	14.9848	15.4654	16.9162	18.2668	19.8091	20.8620	21.1625	21.0938	20.5483	18.8230	16.8966	15.4501
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Net Throughput (gal/mo.):	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667	573,788.1667
Annual Turnovers:	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000	840,000.0000
Maximum Liquid Height (ft):	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000	37.0000
Tank Diameter (ft):	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000	60.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	28.1548	28.8373	34.0746	37.7125	40.6530	39.1633	39.9659	39.0566	36.2652	34.0160	30.7375	28.4080

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	220.28	196.77	417.04

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-7
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Vertical Fixed Roof Tank
Description:	Distillate

Tank Dimensions

Shell Height (ft):	48.00
Diameter (ft):	100.00
Liquid Height (ft):	45.00
Avg. Liquid Height (ft):	22.50
Volume (gallons):	2,741,298.00
Turnovers:	8.20
Net Throughput (gal/yr):	22,470,346.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	0.00
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig):	0.03

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	68.12	62.93	73.30	72.34	0.0084	0.0071	0.0099	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Feb	69.11	63.49	74.73	72.34	0.0087	0.0073	0.0104	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Mar	71.94	65.95	77.92	72.34	0.0095	0.0079	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Apr	74.39	67.88	80.89	72.34	0.0103	0.0084	0.0126	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	May	76.99	70.68	83.30	72.34	0.0112	0.0092	0.0135	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jun	78.67	73.13	84.22	72.34	0.0117	0.0099	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Jul	79.14	73.68	84.59	72.34	0.0119	0.0101	0.0141	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Aug	79.03	73.78	84.28	72.34	0.0119	0.0101	0.0139	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Sep	78.18	73.29	83.08	72.34	0.0116	0.0099	0.0134	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Oct	75.35	70.41	80.28	72.34	0.0106	0.0091	0.0123	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Nov	71.90	66.82	76.98	72.34	0.0095	0.0081	0.0112	130.0000			188.00	Option 5: A=12.101, B=8907
Distillate fuel oil no. 2	Dec	69.08	64.09	74.07	72.34	0.0087	0.0074	0.0102	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	43.8005	44.4695	57.0509	64.6450	69.2794	60.8204	62.4866	59.6934	52.2339	50.5036	46.0204	43.0928
Vapor Space Volume (cu ft):	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Vented Vapor Saturation Factor:	0.9883	0.9879	0.9868	0.9857	0.9846	0.9837	0.9835	0.9836	0.9840	0.9853	0.9868	0.9879
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623	208,457.7623
Tank Diameter (ft):	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000
Vapor Space Outage (ft):	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417
Tank Shell Height (ft):	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000
Average Liquid Height (ft):	22.5000	22.5000	22.5000	22.5000	22.5000	22.5000	22.5000	22.5000	22.5000	22.5000	22.5000	22.5000
Roof Outage (ft):	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417
Roof Outage (Cone Roof)												
Roof Outage (ft):	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417
Roof Height (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0002	0.0002	0.0002	0.0002	0.0003	0.0003	0.0003	0.0003	0.0003	0.0002	0.0002	0.0002
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Daily Avg. Liquid Surface Temp. (deg. R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Average Ambient Temp. (deg. F):	59.7000	61.2000	66.6000	71.2000	76.8500	81.1500	82.3000	82.4500	81.0500	75.2000	68.0000	62.1000
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067	532.0067
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation Factor (Btu/sqft day):	999.0000	1,244.0000	1,582.0000	1,898.0000	1,989.0000	1,831.0000	1,801.0000	1,673.0000	1,497.0000	1,304.0000	1,096.0000	926.0000
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0354	0.0387	0.0412	0.0449	0.0432	0.0374	0.0367	0.0352	0.0326	0.0331	0.0344	0.0339
Daily Vapor Temperature Range (deg. R):	20.7392	22.4814	23.9463	26.0265	25.2356	22.1796	21.8208	20.9955	19.5817	19.7430	20.3370	19.9598
Daily Vapor Pressure Range (psia):	0.0028	0.0031	0.0036	0.0042	0.0044	0.0040	0.0040	0.0038	0.0035	0.0033	0.0031	0.0028
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0071	0.0073	0.0079	0.0084	0.0092	0.0099	0.0101	0.0101	0.0099	0.0091	0.0081	0.0074
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0099	0.0104	0.0115	0.0126	0.0135	0.0139	0.0141	0.0139	0.0134	0.0123	0.0112	0.0102
Daily Avg. Liquid Surface Temp. (deg R):	527.7882	528.7772	531.6072	534.0555	536.6638	538.3436	538.8093	538.7034	537.8510	535.0178	531.5705	528.7462
Daily Min. Liquid Surface Temp. (deg R):	522.6034	523.1569	525.6206	527.5489	530.3549	532.7987	533.3541	533.4545	532.9556	530.0820	526.4862	523.7562
Daily Max. Liquid Surface Temp. (deg R):	532.9730	534.3976	537.5937	540.5622	542.9727	543.8885	544.2645	543.9522	542.7464	539.9536	536.6547	533.7361
Daily Ambient Temp. Range (deg. R):	22.2000	23.0000	22.8000	23.6000	21.9000	18.7000	18.4000	18.1000	17.3000	18.8000	21.0000	21.6000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9883	0.9879	0.9868	0.9857	0.9846	0.9837	0.9835	0.9836	0.9840	0.9853	0.9868	0.9879
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Vapor Space Outage (ft):	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417	26.5417

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	48.9022	50.4704	55.2052	59.6128	64.6460	68.0821	69.0627	68.8386	67.0582	61.4280	55.1413	50.4205
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0084	0.0087	0.0095	0.0103	0.0112	0.0117	0.0119	0.0119	0.0116	0.0106	0.0095	0.0087
Net Throughput (gal/mo.):	1,872,528.833	1,872,528.833	1,872,528.833	1,872,528.833	1,872,528.833	1,872,528.833	1,872,528.833	1,872,528.833	1,872,528.833	1,872,528.833	1,872,528.833	1,872,528.833
	0	0	0	0	0	0	0	0	0	0	0	0
Annual Turnovers:	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970	8.1970
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	2,741,298.000	2,741,298.000	2,741,298.000	2,741,298.000	2,741,298.000	2,741,298.000	2,741,298.000	2,741,298.000	2,741,298.000	2,741,298.000	2,741,298.000	2,741,298.000
	0	0	0	0	0	0	0	0	0	0	0	0
Maximum Liquid Height (ft):	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000
Tank Diameter (ft):	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	92.7026	94.9399	112.2560	124.2577	133.9253	128.9025	131.5492	128.5320	119.2921	111.9316	101.1617	93.5133

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	718.87	654.10	1,372.96

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-8
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Internal Floating Roof Tank
Description:	Gasoline

Tank Dimensions

Diameter (ft):	150.00
Volume (gallons):	5,115,600.00
Turnovers:	18.05
Self Supp. Roof? (y/n):	N
No. of Columns:	9.00
Eff. Col. Diam. (ft):	1.10

Paint Characteristics

Internal Shell Condition:	Light Rust
Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Rim-Seal System

Primary Seal:	Mechanical Shoe
Secondary Seal:	None

Deck Characteristics

Deck Fitting Category:	Detail
Deck Type:	Welded

Deck Fitting/Status	Quantity
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	1
Automatic Gauge Float Well/Bolted Cover, Gasketed	1
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	9
Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed	1
Roof Leg or Hanger Well/Adjustable	58
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Gasoline (RVP 13.5)	Jan	68.12	62.93	73.30	72.34	8.4052	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Feb	69.11	63.49	74.73	72.34	8.5560	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Mar	71.94	65.95	77.92	72.34	8.9991	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Apr	74.39	67.88	80.89	72.34	9.3969	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	May	76.99	70.68	83.30	72.34	9.8358	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Jun	78.67	73.13	84.22	72.34	10.1268	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Jul	79.14	73.68	84.59	72.34	10.2087	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Aug	79.03	73.78	84.28	72.34	10.1900	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Sep	78.18	73.29	83.08	72.34	10.0408	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Oct	75.35	70.41	80.28	72.34	9.5570	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Nov	71.90	66.82	76.98	72.34	8.9932	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Dec	69.08	64.09	74.07	72.34	8.5512	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Rim Seal Losses (lb):	927.6043	953.2470	1,031.9881	1,107.3903	1,196.4966	1,259.4837	1,277.8179	1,273.6136	1,240.5166	1,139.1284	1,030.9122	952.4273
Seal Factor A (lb-mole/ft-yr):	5.8000	5.8000	5.8000	5.8000	5.8000	5.8000	5.8000	5.8000	5.8000	5.8000	5.8000	5.8000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000
Value of Vapor Pressure Function:	0.2079	0.2137	0.2313	0.2482	0.2682	0.2823	0.2864	0.2855	0.2780	0.2553	0.2311	0.2135
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	8.4052	8.5560	8.9991	9.3969	9.8358	10.1268	10.2087	10.1900	10.0408	9.5570	8.9932	8.5512
Tank Diameter (ft):	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Withdrawal Losses (lb):	10.3122	10.3122	10.3122	10.3122	10.3122	10.3122	10.3122	10.3122	10.3122	10.3122	10.3122	10.3122
Number of Columns:	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000
Effective Column Diameter (ft):	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000
Net Throughput (gal/mo.):	7,693,834.833	7,693,834.833	7,693,834.833	7,693,834.833	7,693,834.833	7,693,834.833	7,693,834.833	7,693,834.833	7,693,834.833	7,693,834.833	7,693,834.833	7,693,834.833
	0	0	0	0	0	0	0	0	0	0	0	0
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
Average Organic Liquid Density (lb/gal):	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000
Tank Diameter (ft):	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000
Deck Fitting Losses (lb):	869.0075	913.5831	989.0479	1,061.3126	1,146.7114	1,207.0776	1,224.6489	1,220.6196	1,188.8997	1,091.7302	988.0168	912.7976
Value of Vapor Pressure Function:	0.2079	0.2137	0.2313	0.2482	0.2682	0.2823	0.2864	0.2855	0.2780	0.2553	0.2311	0.2135
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	833.8000	833.8000	833.8000	833.8000	833.8000	833.8000	833.8000	833.8000	833.8000	833.8000	833.8000	833.8000
Deck Seam Losses (lb):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Length (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Loss per Unit Length Factor (lb-mole/ft-yr):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Length Factor(ft/sqft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tank Diameter (ft):	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000	150.0000
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000

Deck Fitting/Status	Quantity	Deck Fitting Loss Factors KFa (lb-mole/yr)	KFb (lb-mole/(yr mph^n))	m	Losses (lb.)
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	1	1.60	0.00	0.00	24.6454
Automatic Gauge Float Well/Bolted Cover, Gasketed	1	2.80	0.00	0.00	43.1294
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	9	33.00	0.00	0.00	4,574.7973
Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed	1	56.00	0.00	0.00	862.5880
Roof Leg or Hanger Well/Adjustable	58	7.90	0.00	0.00	7,057.8186
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1	12.00	0.00	0.00	184.8403
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1	6.20	1.20	0.94	95.5008

Total Losses (lb):	1,826.9240	1,877.1423	2,031.3482	2,179.0151	2,353.5202	2,476.8735	2,512.7789	2,504.5453	2,439.7284	2,241.1707	2,029.2412	1,875.5371

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)				
Components	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Gasoline (RVP 13.5)	13,390.63	123.75	12,833.45	0.00	26,347.82

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	Canaveral Tank-9
City:	Cape Canaveral
State:	Florida
Company:	TransMontaigne Terminaling Inc.
Type of Tank:	Internal Floating Roof Tank
Description:	Gasoline

Tank Dimensions

Diameter (ft):	80.00
Volume (gallons):	1,417,080.00
Turnovers:	18.05
Self Supp. Roof? (y/n):	N
No. of Columns:	5.00
Eff. Col. Diam. (ft):	1.10

Paint Characteristics

Internal Shell Condition:	Light Rust
Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Rim-Seal System

Primary Seal:	Liquid-mounted
Secondary Seal:	Rim-mounted

Deck Characteristics

Deck Fitting Category:	Detail
Deck Type:	Bolted
Construction:	Sheet
Deck Seam:	Sheet: 5 Ft Wide
Deck Seam Len. (ft):	1,005.31

Deck Fitting/Status	Quantity
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	1
Automatic Gauge Float Well/Bolted Cover, Gasketed	1
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	1
Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed	1
Roof Leg or Hanger Well/Adjustable	24
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1
Stub Drain (1-in. Diameter)/	52
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Meteorological Data used in Emissions Calculations: Orlando, Florida (Avg Atmospheric Pressure = 14.75 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Gasoline (RVP 13.5)	Jan	68.12	62.93	73.30	72.34	8.4052	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Feb	69.11	63.49	74.73	72.34	8.5560	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Mar	71.94	65.95	77.92	72.34	8.9991	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Apr	74.39	67.88	80.89	72.34	9.3969	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	May	76.99	70.68	83.30	72.34	9.8358	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Jun	78.67	73.13	84.22	72.34	10.1268	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Jul	79.14	73.68	84.59	72.34	10.2087	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Aug	79.03	73.78	84.28	72.34	10.1900	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Sep	78.18	73.29	83.08	72.34	10.0408	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Oct	75.35	70.41	80.28	72.34	9.5570	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Nov	71.90	66.82	76.98	72.34	8.9932	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3
Gasoline (RVP 13.5)	Dec	69.08	64.09	74.07	72.34	8.5512	N/A	N/A	61.5400			92.00	Option 4: RVP=13.5, ASTM Slope=3

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Rim Seal Losses (lb):	25.5891	26.2965	28.4686	30.5487	33.0068	34.7444	35.2501	35.1342	34.2211	31.4242	28.4390	26.2739
Seal Factor A (lb-mole/ft-yr):	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000
Value of Vapor Pressure Function:	0.2079	0.2137	0.2313	0.2482	0.2682	0.2823	0.2864	0.2855	0.2780	0.2553	0.2311	0.2135
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	8.4052	8.5560	8.9991	9.3969	9.8358	10.1268	10.2087	10.1900	10.0408	9.5570	8.9932	8.5512
Tank Diameter (ft):	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Withdrawal Losses (lb):	5.3699	5.3699	5.3699	5.3699	5.3699	5.3699	5.3699	5.3699	5.3699	5.3699	5.3699	5.3699
Number of Columns:	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000	5.0000
Effective Column Diameter (ft):	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000	1.1000
Net Throughput (gal/mo.):	2,131,280.666	2,131,280.666	2,131,280.666	2,131,280.666	2,131,280.666	2,131,280.666	2,131,280.666	2,131,280.666	2,131,280.666	2,131,280.666	2,131,280.666	2,131,280.666
	0	0	0	0	0	0	0	0	0	0	0	0
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
Average Organic Liquid Density (lb/gal):	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000
Tank Diameter (ft):	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000
Deck Fitting Losses (lb):	387.6746	398.3915	431.2999	462.8128	500.0531	526.3773	534.0397	532.2826	518.4504	476.0771	430.8502	398.0489
Value of Vapor Pressure Function:	0.2079	0.2137	0.2313	0.2482	0.2682	0.2823	0.2864	0.2855	0.2780	0.2553	0.2311	0.2135
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	363.6000	363.6000	363.6000	363.6000	363.6000	363.6000	363.6000	363.6000	363.6000	363.6000	363.6000	363.6000
Deck Seam Losses (lb):	191.0654	196.3472	212.5661	228.0972	246.4511	259.4250	263.2014	262.3354	255.5182	234.6345	212.3445	196.1784
Deck Seam Length (ft):	1,005.3100	1,005.3100	1,005.3100	1,005.3100	1,005.3100	1,005.3100	1,005.3100	1,005.3100	1,005.3100	1,005.3100	1,005.3100	1,005.3100
Deck Seam Loss per Unit Length Factor (lb-mole/ft-yr):	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400
Deck Seam Length Factor(ft/sqft):	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000
Tank Diameter (ft):	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000
Vapor Molecular Weight (lb/lb-mole):	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400	61.5400
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000

Deck Fitting/Status	Quantity	Deck Fitting Loss Factors KFa (lb-mole/yr)	KFb (lb-mole/(yr mph^n))	m	Losses (lb.)
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	1	1.60	0.00	0.00	24.6454
Automatic Gauge Float Well/Bolted Cover, Gasketed	1	2.80	0.00	0.00	43.1294
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	1	33.00	0.00	0.00	508.3108
Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed	1	56.00	0.00	0.00	862.5880
Roof Leg or Hanger Well/Adjustable	24	7.90	0.00	0.00	2,920.4767
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1	12.00	0.00	0.00	184.8403
Stub Drain (1-in. Diameter)/	52	1.20	0.00	0.00	961.1695
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1	6.20	1.20	0.94	95.5008

Total Losses (lb):	609.6990	626.4051	677.7045	726.8286	784.8809	825.9166	837.8612	835.1222	813.5597	747.5058	677.0036	625.8711

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)				
Components	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Gasoline (RVP 13.5)	369.40	64.44	5,596.36	2,758.16	8,788.36

TANKS 4.0
Emissions Report - Detail Format
Total Emissions Summaries - All Tanks in Report

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

Tank Identification				Losses (lbs)
Canaveral Tank-1	TransMontaigne Terminaling Inc.	Vertical Fixed Roof Tank	Cape Canaveral, Florida	1,690.14
Canaveral Tank-10	TransMontaigne Terminaling Inc.	Vertical Fixed Roof Tank	Cape Canaveral, Florida	63.89
Canaveral Tank-11	TransMontaigne Terminaling Inc.	Vertical Fixed Roof Tank	Cape Canaveral, Florida	63.89
Canaveral Tank-12	TransMontaigne Terminaling Inc.	Vertical Fixed Roof Tank	Cape Canaveral, Florida	185.27
Canaveral Tank-13	TransMontaigne Terminaling Inc.	Internal Floating Roof Tank	Cape Canaveral, Florida	5,490.48
Canaveral Tank-14	TransMontaigne Terminaling Inc.	Vertical Fixed Roof Tank	Cape Canaveral, Florida	31.54
Canaveral Tank-15	TransMontaigne Terminaling Inc.	External Floating Roof Tank	Cape Canaveral, Florida	7,433.01
Canaveral Tank-17	TransMontaigne Terminaling Inc.	Internal Floating Roof Tank	Cape Canaveral, Florida	26,278.11
Canaveral Tank-18	TransMontaigne Terminaling Inc.	Internal Floating Roof Tank	Cape Canaveral, Florida	26,277.55
Canaveral Tank-2	TransMontaigne Terminaling Inc.	Vertical Fixed Roof Tank	Cape Canaveral, Florida	1,232.59
Canaveral Tank-23	TransMontaigne Terminaling Inc.	Horizontal Tank	Cape Canaveral, Florida	5.37
Canaveral Tank-24A	TransMontaigne Terminaling Inc.	Horizontal Tank	Cape Canaveral, Florida	4.63
Canaveral Tank-3	TransMontaigne Terminaling Inc.	Vertical Fixed Roof Tank	Cape Canaveral, Florida	723.21
Canaveral Tank-4	TransMontaigne Terminaling Inc.	Vertical Fixed Roof Tank	Cape Canaveral, Florida	417.04
Canaveral Tank-5	TransMontaigne Terminaling Inc.	Vertical Fixed Roof Tank	Cape Canaveral, Florida	25.49
Canaveral Tank-6	TransMontaigne Terminaling Inc.	Vertical Fixed Roof Tank	Cape Canaveral, Florida	417.04
Canaveral Tank-7	TransMontaigne Terminaling Inc.	Vertical Fixed Roof Tank	Cape Canaveral, Florida	1,372.96
Canaveral Tank-8	TransMontaigne Terminaling Inc.	Internal Floating Roof Tank	Cape Canaveral, Florida	26,347.82
Canaveral Tank-9	TransMontaigne Terminaling Inc.	Internal Floating Roof Tank	Cape Canaveral, Florida	8,788.36
Total Emissions for all Tanks:				106,848.40

EMISSIONS TESTING
of the
COASTAL FUELS MARKETING. INC.
PORT CANAVERAL TERMINAL
VAPOR COMBUSTION UNIT
Port Canaveral, FL

August 26, 2003

FDEP Permit No. 0090029-003-AV
SES Reference No. 03S301

Conducted by:

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EMISSIONS TESTING

EMISSIONS TESTING
of the
COASTAL FUELS MARKETING. INC.
PORT CANAVERAL TERMINAL
VAPOR COMBUSTION UNIT

Port Canaveral, FL

August 26, 2003

TABLE OF CONTENTS

1.0 INTRODUCTION

Southern Environmental Sciences, Inc. conducted a flare emissions test and visible emissions evaluation of the Coastal Fuels Marketing, Inc., Port Canaveral Terminal, Vapor Combustion Unit on August 26, 2003. This facility is located at Port Canaveral, Florida. Testing was performed to determine if the plant was operating in compliance with requirements of the Florida Department of Environmental Protection (FDEP). Mr. Thomas Mulligan of the FDEP was present as an observer during a portion of the test.

2.0 SUMMARY OF RESULTS

The flare was found to be in compliance with applicable emission limiting standards. Results of the test are summarized in Table 1. Emissions from the vapor collection system due to the loading of liquid product into gasoline tank trucks is limited to 35 milligrams of volatile organic compounds per liter of gasoline loaded. The emission rate during the test was 9.01 milligrams of volatile organic compounds per liter of gasoline loaded, within the allowable limit. The maximum allowable vapor system pressure, measured at each loading rack vapor recovery line is 17.7 inches of water. The maximum pressure observed during the test was 3.5 inches of water. A visual determination of fugitive emissions was performed over a two hour period. The accumulated emission time was zero minutes, well within the maximum limit of 5 minutes during any 2 consecutive hours.

TABLE 1. EMISSIONS TEST SUMMARY

Company: COASTAL FUELS - PORT CANAVERAL
Source: VAPOR COMBUSTION UNIT

Date of Test	08/26/2003
Start Time (24-hr. clock)	0635
End Time (24-hr. clock)	1235
Inlet Gas Volume (SCM)	705
Outlet Gas Volume (SCM)	76,040
Average Barometric Pressure (in. Hg.)	30.06
Average Static Pressure (in. H2O)	0.7
Average Meter Temperature (`F)	90
Gas Meter Correction Factor	1
Total Loading Positions	3
Total Trucks Checked	13
Trucks With Leaks	0
Trucks With No Leaks	13
Total Gasoline Dispensed (gallons)	101,680
Gasoline excluded Due to Leaks (gallons)	0
Total Countable Gasoline Dispensed (gallons)	101,680
Total Countable Gasoline Dispensed (liters)	384,859

Average VOC Inlet Concentration, (ppm, as propane)	256,014
Total mass of Inlet Hydrocarbons, (milligrams as carbon)	364,003,677
Average VOC Outlet Concentration, (ppm, as propane)	21.5
Average CO Outlet Concentration, (ppm)	63.0
Average CO2 Outlet Concentration, (%)	0.8
Total mass of Outlet Hydrocarbons, (milligrams as carbon)	3,469,155
Average Efficiency, (%)	98.5
Emission rate (mg/l)	**9.01**
Allowable Emission rate (mg/l)	**35**

3.0 PROCESS DESCRIPTION

The Coastal Fuels Marketing, Inc., Port Canaveral Terminal truck loading facility controlled by this vapor combustion unit includes one loading rack. Trucks are bottom filled to reduce the amount of vapors generated. The displaced vapors are routed through an air assisted flare. The amount of product loaded during the testing period was monitored by Coastal Fuels personnel and is included in Table 1.

4.0 TESTING PROCEDURES

4.1 Methods

Flare testing and analyses were conducted in accordance with procedures described in 40 CFR 60.503 and 60.18. Volumetric flowrate at the inlet and outlet were determined in accordance with EPA Method 2B - Determination of Exhaust Gas Volume Flow Rate from Gasoline Vapor Incinerators, 40 CFR 60, Appendix A-1. Hydrocarbon concentrations were measured at the inlet and outlet in accordance with EPA Method 25A - Determination of Total Gaseous Organic Concentration Using a Flame Ionization Analyzer, 40 CFR 60, Appendix A-7. Carbon monoxide concentration was measured at the outlet in accordance with EPA Method 10 - Determination of Carbon Monoxide Emissions from Stationary Sources, 40 CFR 60, Appendix A-4. Carbon dioxide was also measured at the outlet using procedures generally described in Method 10 by substituting carbon dioxide gas where the method called for carbon monoxide and omitting the silica gel and carbon dioxide absorbent tubes. The inlet total hydrocarbon analyzer, the carbon monoxide and the

carbon dioxide analyzers were calibrated with an Environics Model 2020 gas dilution system and calibration gases using procedures described in EPA Method 205 - Verification of Gas Dilution Systems for Field Instrument Calibrations, 40 CFR 51, Appendix M. Trucks were checked for leaks using procedures described in EPA Method 21 - Determination of Volatile Organic Compound Emission Leaks, 40 CFR 60, Appendix A-7. The visual determination of fugitive emissions was performed in accordance with EPA Method 22 - Visual Determination of Fugitive Emissions from Material Sources and Smoke Emissions from Flares, 40 CFR 60, Appendix A-7.

4.2 Pretest Preparation

Prior to testing, an eight inch American Meter Company turbine meter was connected in line to measure the total volume of vapor reaching the flare. The vapor flare, terminal vapor recovery lines and testing ductwork were checked for leaks with a combustible gas detector. Any leaks detected were repaired prior to testing. Magnehelic gauges were connected at each loading rack to measure the vapor collection system pressure. Two Gastech Model GT 105 combustible gas detectors were calibrated prior to the test with zero air and 2.5 percent methane calibration gas. Each analyzer was calibrated in accordance with the applicable test method immediately prior to the test.

4.3 Sampling Trains

The inlet Method 25A sampling train consisted of a dilution probe (100:1), a teflon

sample line, heated as necessary to prevent condensation, a California Analytical Model 300HFID(M) heated total hydrocarbon analyzer and a strip chart recorder. The Outlet Method 25A sampling train consisted of a heated stainless steel probe, heated teflon sample line, a California Analytical Model 300HFID(M) heated total hydrocarbon analyzer and a strip chart recorder. A schematic of the hydrocarbon sampling train is shown in Figure 1. The carbon monoxide sampling train consisted of a heated stainless steel probe, condenser, silica gel tube, carbon dioxide absorption tube, teflon sample line, and a Thermo Environmental Instruments, Inc. Model 48 Gas Filter Correlation CO analyzer. A schematic of the carbon monoxide sampling train is shown in Figure 2. The carbon dioxide sampling train consisted of a heated stainless steel sampling probe, condenser, teflon sample line and a California Analytical Model 100 carbon dioxide analyzer.

4.4 Data Collection

Inlet volume, temperature and static pressure measurements were recorded at the inlet to the meter at five minute intervals for the duration of the test to determine volume at standard conditions. Inlet and outlet hydrocarbon concentrations and outlet carbon monoxide and carbon dioxide concentrations were measured continuously throughout the six hour test period. During the testing each applicable tank truck was tested for leaks at all domes and boots. The probe of the gas meter

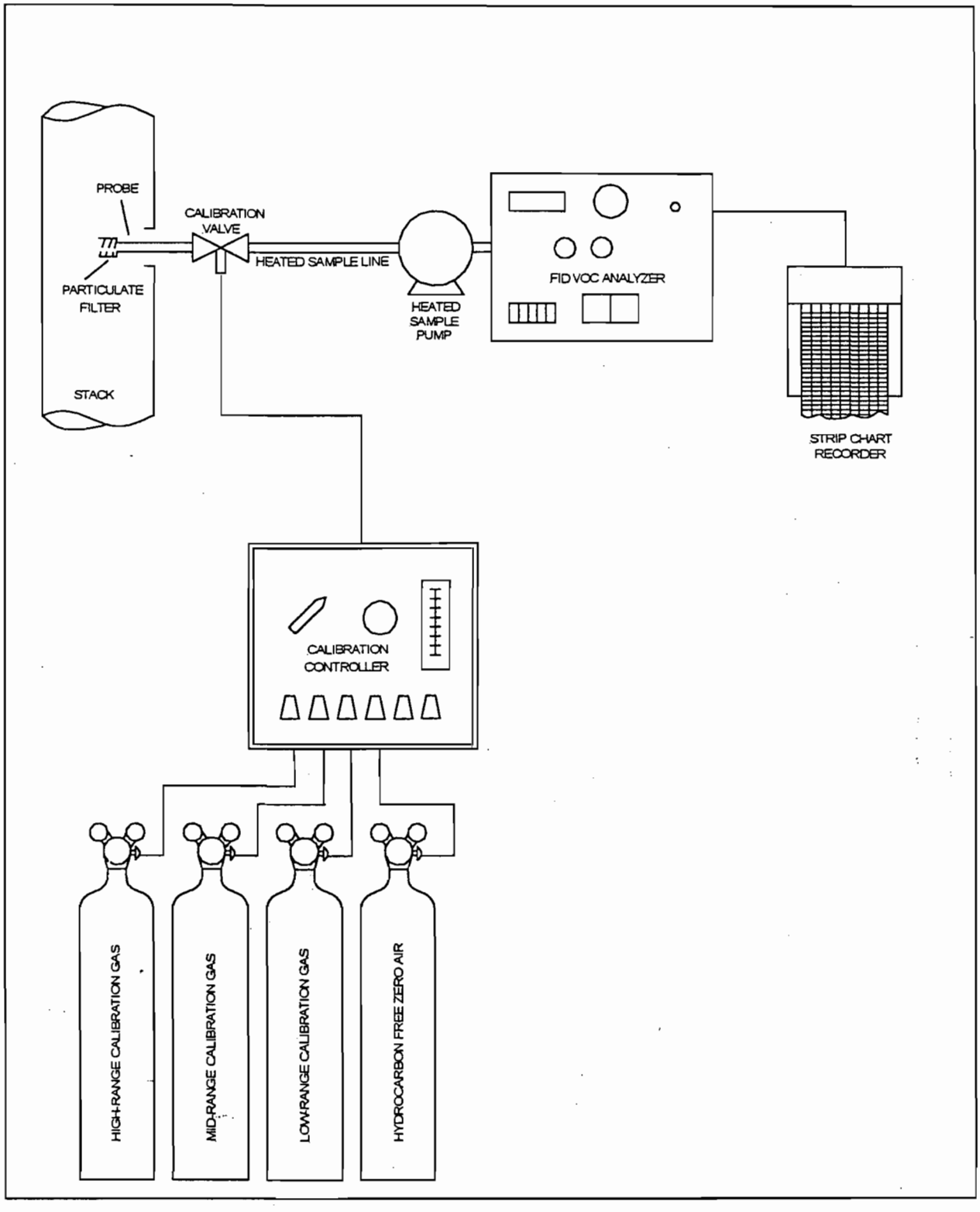


Figure 1. EPA Method 25A Sampling Train

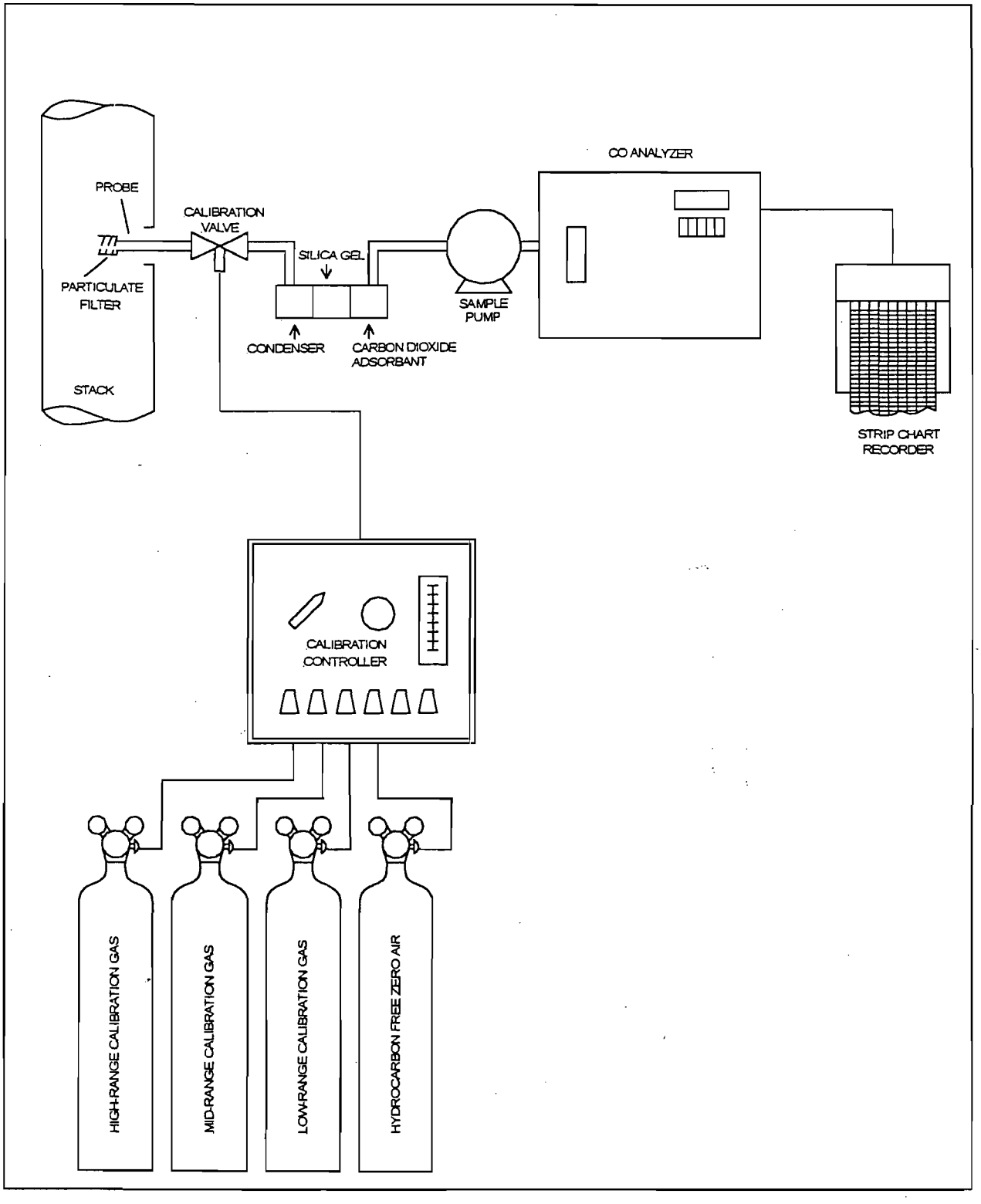


Figure 2. EPA Method 10 Sampling Train.

was held 2.5 centimeters from the potential leak source and probe movement was maintained at 2 centimeters per second. If an increase in concentration was noted at a possible leak, the probe was moved to locate the point of highest meter response. Leaks greater than or equal to 10,000 parts per million (as methane) were documented on field data sheets.

5.0 ANALYTICAL PROCEDURE

5.1 Analysis

Within 2 hours of the start of the test zero and high-level propane calibration gases were introduced into the hydrocarbon analyzers at the calibration valve assembly and the output was adjusted to the appropriate level if necessary. A linear regression was then conducted to calculate the predicted response for the low-level and mid-level gases. The low-level and mid-level gases were then introduced into the measurement system. The difference between the predicted and actual responses were calculated. A difference of less than 5 percent was considered acceptable. To assess the response time of the measurement system, zero gas was introduced into the system. After the output was stabilized, the high-level gas was quickly introduced. The time from the concentration change to the measurement system response equivalent to 95 percent of the step change was determined. The test was repeated three times. Results were recorded on the appropriate strip charts and are included in the appendix. Instrument calibrations were checked periodically during the test by introducing mid-range and zero gases into the instrument through the sampling train. The carbon

monoxide and carbon dioxide analyzers were calibrated immediately before the beginning of the test and checked periodically by introducing mid-range and zero gases into the instruments through the sampling trains.

5.2 Data Reduction

The outlet volume was determined in accordance with equations in EPA Method 2B. Hydrocarbon emissions were determined from the outlet hydrocarbon concentrations and the calculated outlet flowrate. The total countable gasoline loaded during the test was calculated by summing the total gasoline loaded then subtracting the total loaded into trucks on which leaks were encountered.

APPENDIX

Project Participants

Certification

Visual Determination of Fugitive Emissions

Laboratory Data

Field Data Sheets

Calculations and Equations

Strip Charts

Calibration Data

PROJECT PARTICIPANTS AND CERTIFICATION

COASTAL FUELS MARKETING. INC.
CAPE CANAVERAL TERMINAL
VAPOR COMBUSTION UNIT

Port Canaveral, FL

August 26, 2003

Project Participants:

Kenneth M. Roberts Mark. S. Gierke Terry L. Wilson Dale A. Wingler	Conducted the field testing.
Dale A. Wingler	Performed the visual determination of fugitive emissions.
Kenneth M. Roberts	Computed test results.
Kenneth M. Roberts	Prepared the final test report.

Certification:

I certify that to my knowledge all data submitted in this report is true and correct.

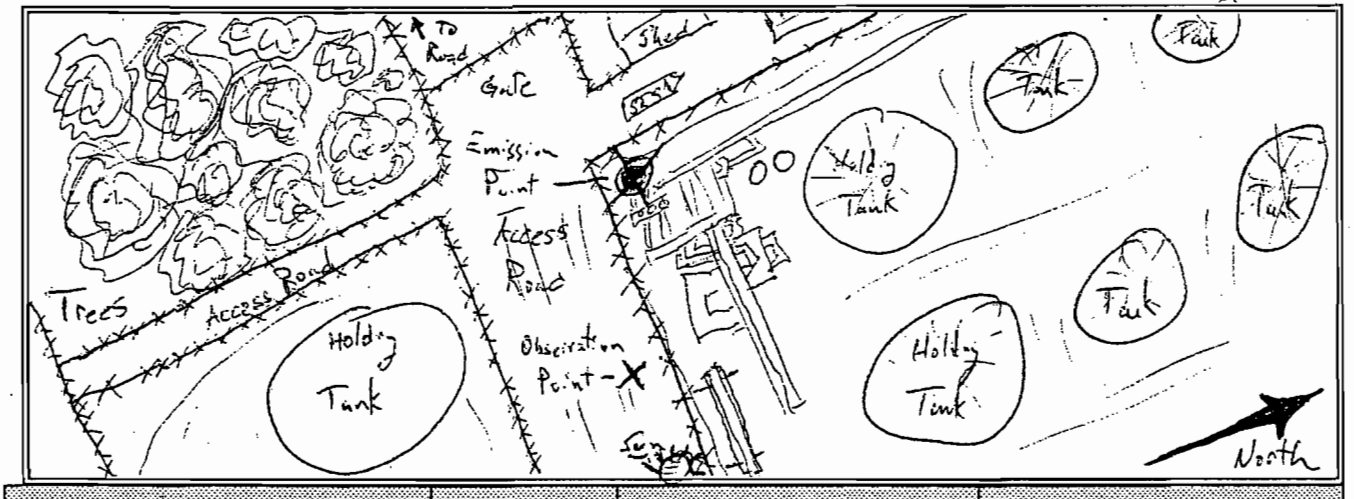
Kenneth M. Roberts, QEP

SOUTHERN ENVIRONMENTAL SCIENCES, INC.

EPA METHOD 22
FUGITIVE OR SMOKE EMISSION INSPECTION
OUTDOOR LOCATION

COMPANY	Coastal Fuels	DATE	8/26/03
UNIT	Port Canaveral	SKY CONDITIONS	Scattered
PERMIT NO.	0090029-003-AV	PRECIPITATION	None
OBSERVER	Dale A. Gwinder	WIND DIRECTION	Variable
AFFILIATION	SES	WIND SPEED	0-3
INDUSTRY	Gasoline Terminal	PROCESS UNIT	Shrouded Flare

Sketch process unit: indicate observer position relative to source and sun: indicate potential emission points and/or actual emission points.



OBSERVATIONS	CLOCK TIME	OBSERVATION PERIOD DURATION (MIN:SEC)	ACCUMULATED EMISSION TIME* (MIN:SEC)
BEGIN OBSERVATION	0718-0738	20:00	00:00
	0743-0803	20:00	00:00
	0808-0828	20:00	00:00
	0833-0853	20:00	00:00
	0858-0918	20:00	00:00
	0923-0943	20:00	00:00
END OBSERVATION			

* Last reading indicates total duration of observed emissions for the test.

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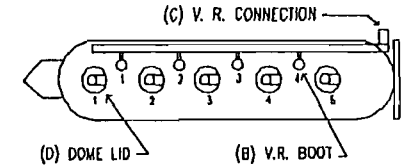
(1)



LEAK LOCATION DIAGRAM

TRUCK LEAK CHECKS			
COMPANY	Coastal Fuels	DATE	8/26/03
LOCATION	Port Canaveral	OPERATOR(S)	DW / TW
FACILITY	Flare	INSTRUMENT(S)	GT 105

OWNER	TRUCK NO.	TIME	RACK NO.	LANE NO.	V.R.BACK PRESSURE (IN. H2O)		GALLONS LOADED	PRODUCT THIS LOAD	PRODUCT PREV LOAD	NO LEAK	LEAK	LEAK LOCATION
Florida Rock	9772	0627	/	1	1.0	1	7500	Diesel				
						2						
						3						
						4						
					TOTAL							
FleetWing	141	0628	/	2	2.0	1	3800	Diesel				
						2						
						3						
						4						
					TOTAL							
FleetWing	143	0631	/	3	1.5	1	4160	Diesel				
						2						
						3						
						4						
					TOTAL							
RC Dunn Mobil	15	0651	/	2	1.5	1	5000	Diesel				
						2						
						3						
						4						
					TOTAL							
Penn Tank Lines, Inc.	9587	0708	/	1	1.5	1	7900	Diesel				
						2						
						3						
						4						
					TOTAL							

TRKLEAK.FRM

(2)

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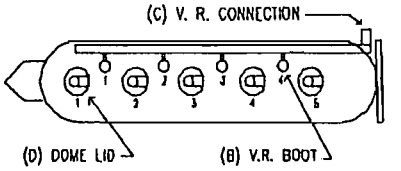

LEAK LOCATION DIAGRAM

TRUCK LEAK CHECKS			
COMPANY	Coastal Fuels	DATE	4/26/03
LOCATION	Port Canaveral	OPERATOR(S)	DW/TW
FACILITY	Flare	INSTRUMENT(S)	GT 105

OWNER	TRUCK NO.	TIME	RACK NO.	LANE NO.	V.R.BACK PRESSURE (IN. H2O)		GALLONS LOADED	PRODUCT THIS LOAD	PRODUCT PREV LOAD	NO LEAK	LEAK	LEAK LOCATION
Kinan	1303	0725	/	2	3.5	1	3100	87	Gas	✓		
						2	2100	93	1			
						3	2800	Dies.		1		
						4						
						TOTAL	~~8000~~ — 5500 Gals					
RC Dunn	15	✓ 0747	/	2	1.5	1	4682	Diesel	Dies			
						2						
						3						
						4						
						TOTAL						
Petro chemical	6129	0800	/	3	2.5	1	8000	87	Gas	✓		
						2	1000	93	1			
						3				1		
						4						
						TOTAL	— 9000					
Fla Rock	RN 9935	0800	/	1	2.5	1	7000	87	Dies	✓		
						2	2000	Dies				
						3				1		
						4						
						TOTAL	— 7000					
PCT	8443	0807	/	2	3.5	1						
						2	5000	87	Gas			
						3	4000	87	1			
						4						
						TOTAL	— 9000					

(3)

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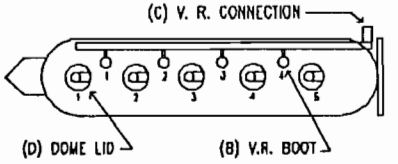

LEAK LOCATION DIAGRAM

TRUCK LEAK CHECKS			
COMPANY	Coastal Fuels	DATE	8/26/03
LOCATION	Port Canaveral	OPERATOR(S)	MG / TW
FACILITY	Flare	INSTRUMENT(S)	GT 105

OWNER	TRUCK NO.	TIME	RACK NO.	LANE NO.	V.R.BACK PRESSURE (IN. H2O)		GALLONS LOADED	PRODUCT: THIS LOAD	PRODUCT: PREV LOAD	NO LEAK	LEAK	LEAK LOCATION
Petro chem.	763994	0818	/	1	2.0	1	5000	87	Gas	✓		
						2	3000	87	1	1		
						3						
						4						
					TOTAL	—	8000					
Florida Rock & Tank Lines	9772	~~0830~~ 0853	/	~~2~~ 2	2.5	1	8000	Rev	Diesel	✓		
						2	1000	93	1	1		
						3						
						4	9000					
					TOTAL							
PCT	6116	0904	/	3	2.0	1	7000	87	Gas	✓		
						2	1000	93				
						3	1000	89	1	1		
						4						
					TOTAL	—	9000					
Fla Rock Tank Lines	3370	0925	/	2	2.0	1	8000	89	Gas	✓		
						2	1000	93		1		
						3						
						4						
					TOTAL	—	9000					
Glover Oil Co.	—	0944	/	3	2.0	1						
						2	345	89	Gas			
						3	1500	87	Dies			
						4						
					TOTAL							

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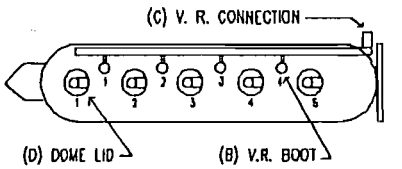


LEAK LOCATION DIAGRAM

TRUCK LEAK CHECKS			
COMPANY		DATE	
LOCATION		OPERATOR(S)	
FACILITY		INSTRUMENT(S)	

OWNER	TRUCK NO.	TIME	RACK NO.	LANE NO.	V.R.BACK PRESSURE (IN. H2O)		GALLONS LOADED	PRODUCT: THIS LOAD	PRODUCT: PREV LOAD	NO LEAK	LEAK	LEAK LOCATION
Watkins Oil Co.	2	0950	/	1	2.0	1	4200	Diesel				
						2						
						3						
						4						
						TOTAL						
Petro-Chemical Transport, Inc.	TC3948 ~~6335~~	~~1011~~ 1021	/	2	2.0	1	~~7000~~	~~Reg~~	✓			
						2	~~1400~~ 500	~~Prem~~ Reg				
						3	2500	Mid	1			
						4	1000	Prem				
						TOTAL	8500					
Kenan	335	1011	/	3	2.0	1	7000	Reg	✓			
						2	1800	Prem				
						3			1			
						4						
						TOTAL	8800					
Petro-Chemical Transport, Inc	6129	1025	/	1	2.0	1	5000	Reg	✓			
						2	4000	Mid				
						3			1			
						4						
						TOTAL	9000					
Florida Rock & Tank Lines	RW 9935	1048	/	3	3.0	1	~~8000~~	Reg	✓			
						2	800	Mid				
						3			1			
						4						
						TOTAL	8800					

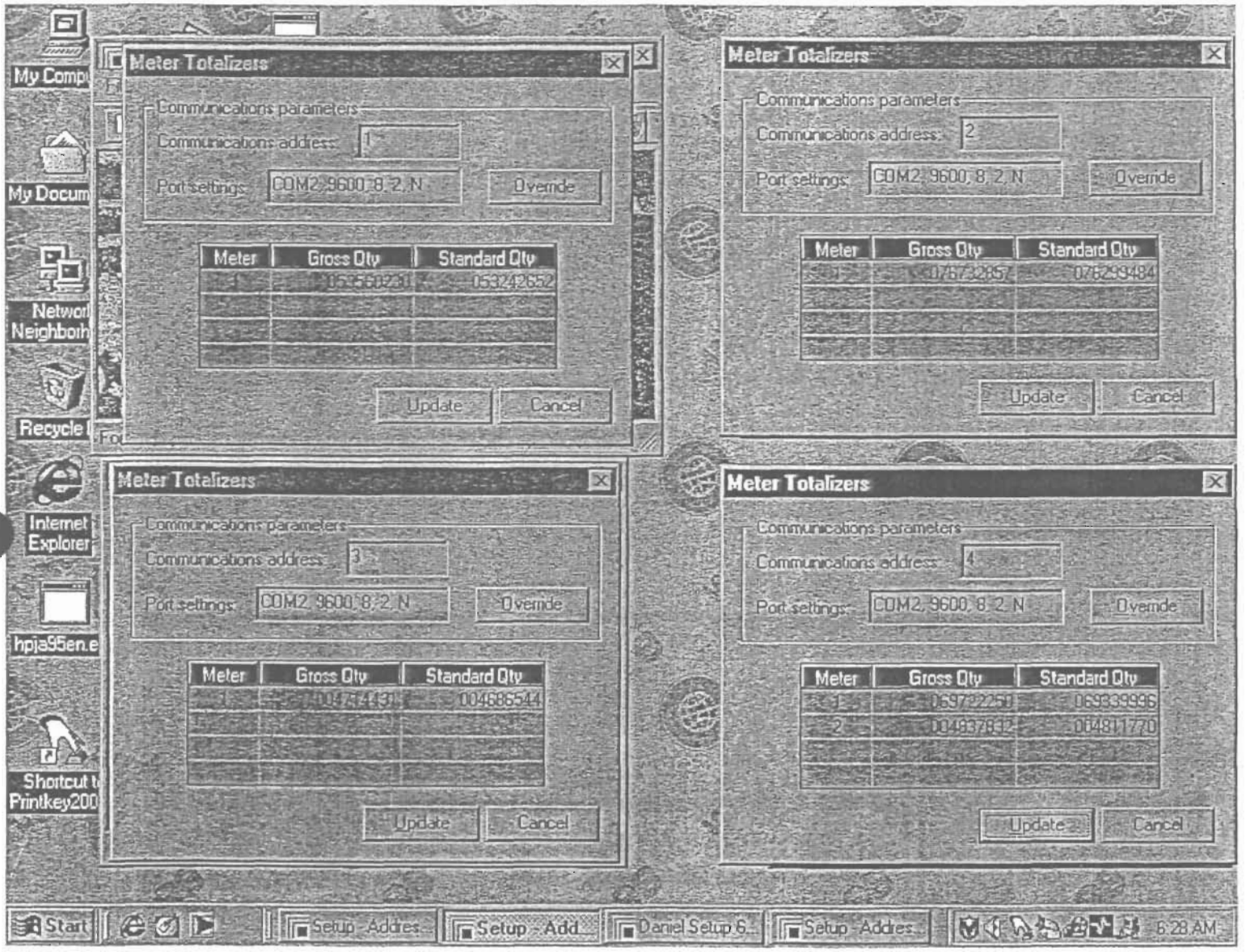
PRODUCT DISPENSED

COMPANY: COASTAL FUELS - PORT CANAVERAL
FACILITY: FLARE
DATE: 08/26/2003

LOCATION NO	METER NO	PRODUCT	PRODUCT INITIAL	PRODUCT FINAL	STATION	RACK TOTALS DIESEL	RACK TOTALS GASOLINE
1	1	LSD	53560230	53588731	28,501		
2	1	RNL	76732857	76745567	12,710		
3	1	SNL	4714431	4714431	0		
4	1	RNL	69722250	69733550	11,300		
4	2	SNL	4837832	4837832	0	28,501	24,010
5	1	LSD	45726247	45757210	30,963		
6	1	RNL	66482028	66504530	22,502		
7	1	SNL	18839350	18842750	3,400		
8	1	RNL	59119623	59132650	13,027		
8	2	SNL	3786399	3788475	2,076	30,963	41,005
9	1	LSD	13458561	13467896	9,335		
10	1	RNL	85422765	85440566	17,801		
11	1	SNL	23565467	23569470	4,003		
12	1	RNL	484969	499352	14,383		
12	2	SNL	54262	54740	478	9,335	36,665

TOTAL PRODUCT DISPENSED (GALLONS)	170,479
TOTAL DIESEL DISPENSED (GALLONS)	68,799
TOTAL GASOLINE DISPENSED (GALLONS)	101,680
TOTAL GASOLINE DISPENSED (LITERS)	384,859

VAPOR TEST

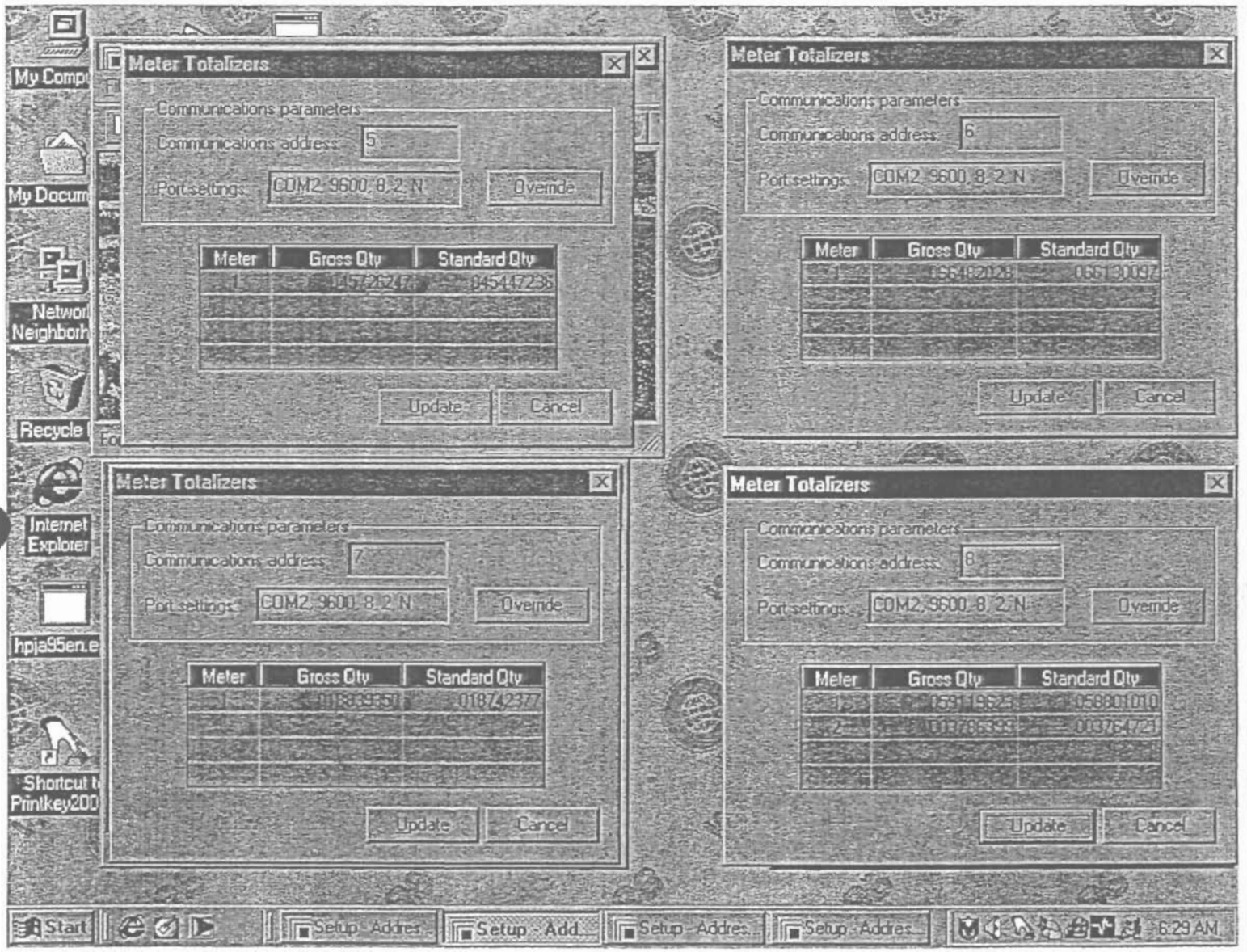


START
Page1

RNL

SNL

LSD



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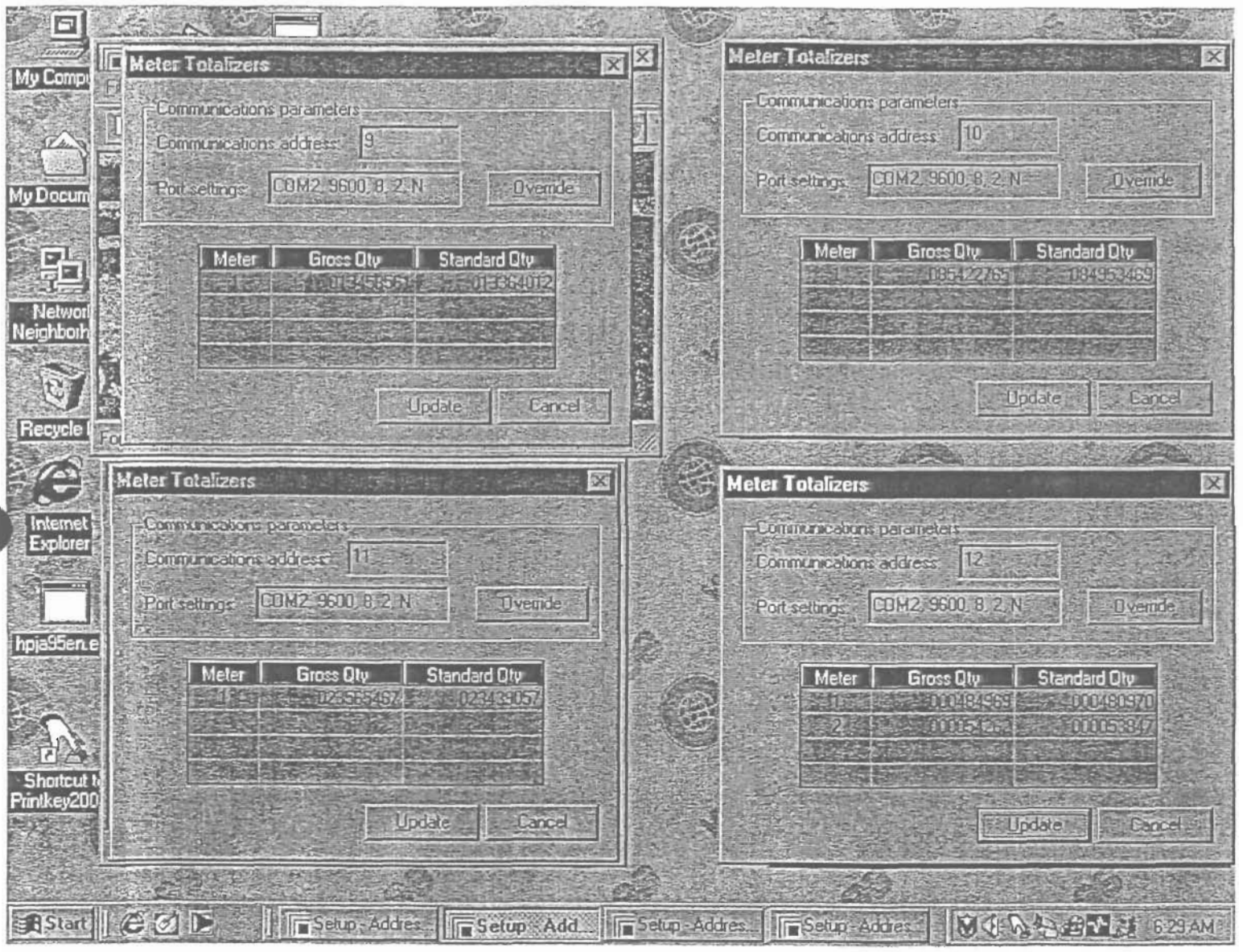
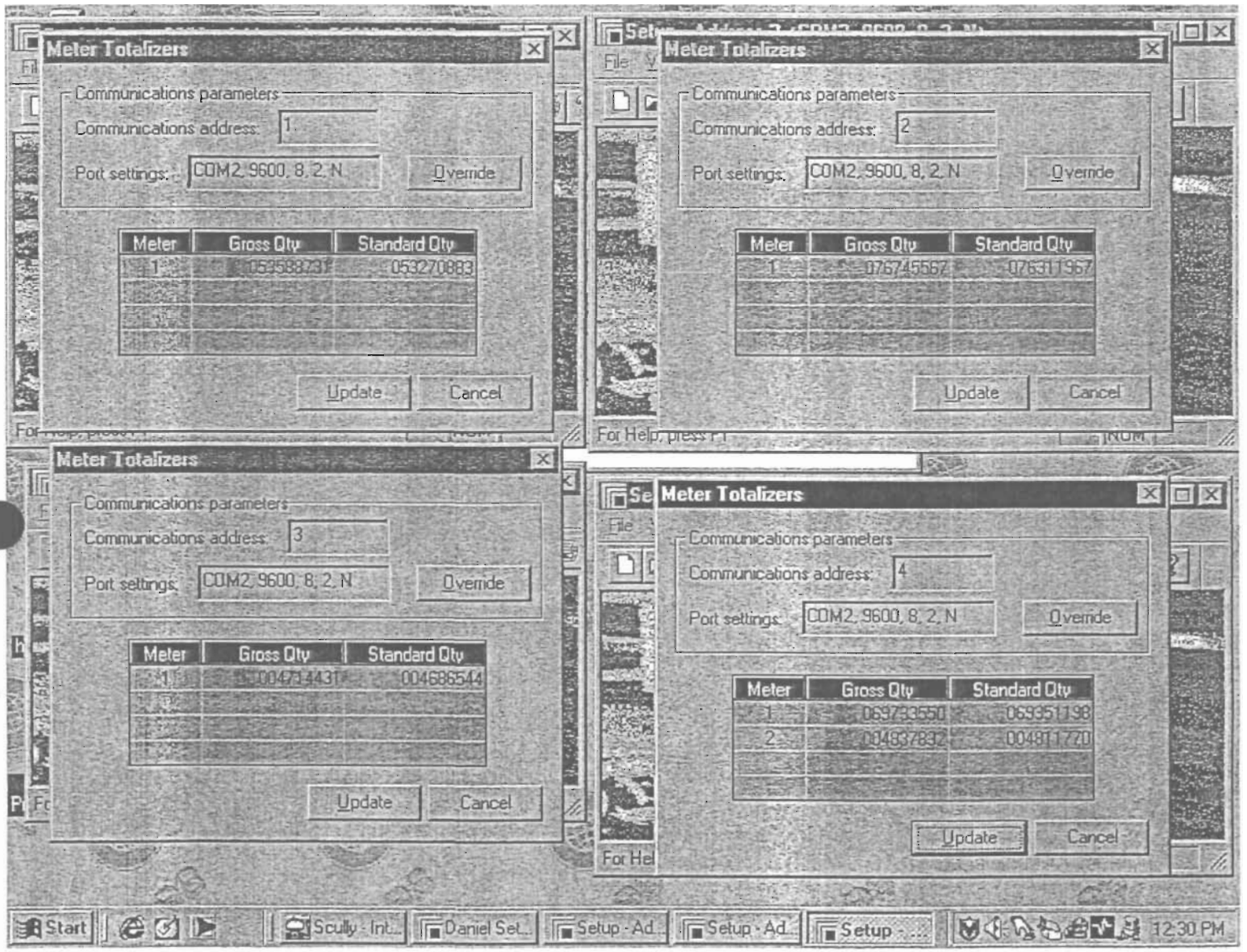
Page 2



Start A
Page 3

VAPOR TEST



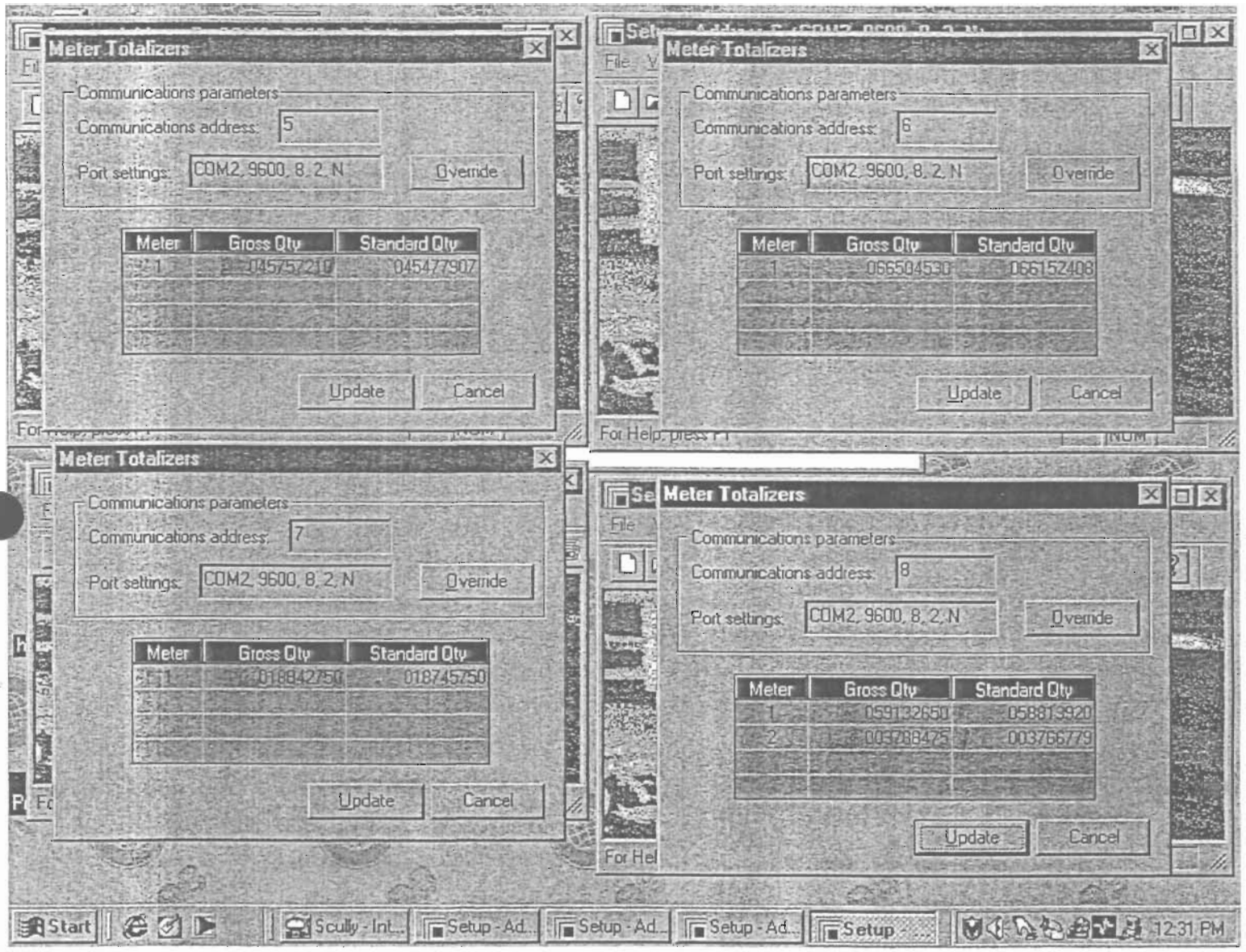
LSD = 68,799 DR. GALS.

SNL = 9,957 DR. GALS.

RUNL = 91,723 DR. GALS.

FINISH

Page 1



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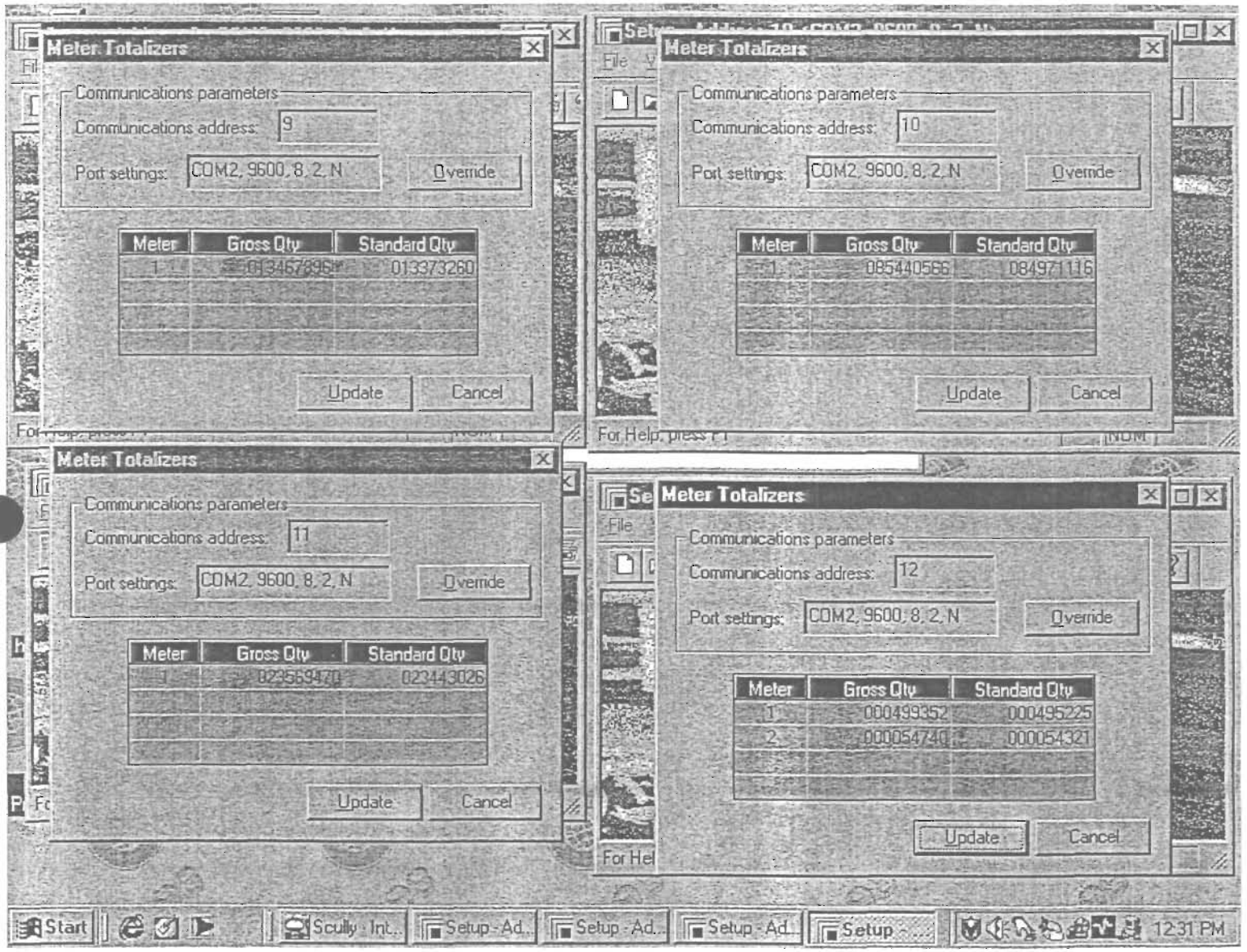

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Page 3

VRU EMISSION CALCULATIONS

COMPANY: COASTAL FUELS - PORT CANAVERAL
FACILITY: VAPOR COMBUSTION UNIT
DATE: 08/26/2003

TIME (min)	METER RDG. cf #1	STATIC PRESSURE ("H2O)	METER TEMP. (deg f)	BAROM. PRESSURE ("Hg)	INLET VOC, (AS PROPANE)			OUTLET VOC, (AS PROPANE)			CARBON MONOXIDE			CARBON DIOXIDE			INLET		OUTLET		FLARE CONTROL EFF. (%)
					ANALYZER READING (% CHART)	INSTRU. SCALE (%)	CONC. (%)	ANALYZER READING (% CHART)	INSTRU. SCALE (PPM)	CONC. (PPM)	ANALYZER READING (% CHART)	INSTRU. SCALE (PPM)	CONC. (PPM)	ANALYZER READING (% CHART)	INSTRU. SCALE (%)	CONC. (%)	GAS VOLUME (M3)*	MASS (mg)	GAS VOLUME (M3)*	MASS (mg)	
0																					
5	1100	1	73	30.05	20	100	20	0	1,000	0	0.5	1,000	5	2	20	0.4	31.07	11,390,041	5031.48	0	100.00
10	1600	1	73	30.05	8	100	8	0	1,000	0	0.5	1,000	5	1	20	0.2	14.12	2,070,917	1987.91	0	100.00
15	1700	1	73	30.05	6	100	6	2	1,000	20	0.5	1,000	5	1	20	0.2	2.82	310,637	288.05	10,560	96.60
20	2000	1	72	30.05	5	100	5	3	1,000	30	0.5	1,000	5	1	20	0.2	8.49	778,053	709.42	39,011	94.99
25	2200	1	72	30.05	4.5	100	4.5	2	1,000	20	0.5	1,000	5	1	20	0.2	5.66	466,832	432.89	15,870	96.60
30	2400	0.5	73	30.05	4	100	4	2	1,000	20	0.5	1,000	5	1	20	0.2	5.64	413,678	383.60	14,063	96.60
35	2500	0.5	73	30.05	3.8	100	3.8	2	1,000	20	0.5	1,000	5	1	20	0.2	2.82	196,497	182.21	6,680	96.60
40	2700	0.8	73	30.05	8	100	8	3	1,000	30	0.5	1,000	5	1	20	0.2	5.65	827,962	754.93	41,513	94.99
45	2900	0.8	73	30.05	21	100	21	4	1,000	40	1.5	1,000	15	1	20	0.2	5.65	2,173,401	1938.49	142,130	93.46
50	3200	0.6	74	30.05	33	100	33	3	1,000	30	5	1,000	50	2.5	20	0.5	8.45	5,110,925	1728.28	95,038	98.14
55	3600	0.5	74	30.05	37.5	100	37.5	1.5	1,000	15	9	1,000	90	3.5	20	0.7	11.26	7,741,934	1853.83	50,971	99.34
60	4100	1	75	30.05	40	100	40	4.5	1,000	45	12	1,000	120	7	20	1.4	14.07	10,315,874	1209.86	99,795	99.03
65	4800	0.5	75	30.05	44	100	44	2	1,000	20	17	1,000	170	6	20	1.2	19.67	15,867,057	2176.78	79,801	99.50
70	4800	0.5	75	30.05	45	100	45	2	1,000	20	1	1,000	10	2	20	0.4					
75	4900	1	76	30.05	44	100	44	1	1,000	10	1.5	1,000	15	4	20	0.8	2.81	2,265,258	478.69	8,774	99.61
80	5200	1	76	30.05	22	100	22	2	1,000	20	8	1,000	80	4	20	0.8	8.43	3,397,887	709.34	26,004	99.23
85	5400	1	76	30.05	12	100	12	1.5	1,000	15	5	1,000	50	2.5	20	0.5	5.62	1,235,595	421.74	11,596	99.06
90	6200	2	76	30.05	10	100	10	2	1,000	20	4	1,000	40	3	20	0.6	22.52	4,128,704	1165.05	42,711	98.97
95	7000	1	77	30.05	18	100	18	3.5	1,000	35	6	1,000	60	5	20	1	22.43	7,399,767	1227.66	78,761	98.94
100	7700	1	78	30.05	35	100	35	3.5	1,000	35	15	1,000	150	6	20	1.2	19.59	12,566,479	1720.37	110,371	99.12
105	7900	0.5	79	30.05	43	100	43	0.5	1,000	5	8	1,000	80	4	20	0.8	5.58	4,397,533	923.32	8,462	99.81
110	7900	0.5	80	30.05	43	100	43	2	1,000	20	1	1,000	10	1.5	20	0.3					
115	8100	1	78	30.05	42	100	42	3	1,000	30	3	1,000	30	2	20	0.4	5.60	4,308,507	1845.96	101,509	97.64
120	9100	1	79	30.05	46	100	46	3	1,000	30	20	1,000	200	8	20	1.6	27.93	23,550,432	2410.51	132,554	99.44
125	9700	1	79	30.07	41	100	41	2.5	1,000	25	15	1,000	150	6	20	1.2	16.77	12,602,723	1729.68	79,262	99.37
130	10200	1	80	30.07	34	100	34	2.5	1,000	25	15	1,000	150	5	20	1	13.95	8,693,071	1433.51	65,691	99.24
135	10600	0.5	82	30.07	42	100	42	1	1,000	10	13	1,000	130	4.5	20	0.9	11.10	8,548,660	1579.15	28,946	99.66
140	10600	1	82	30.07	46.5	100	46.5	1	1,000	10	10	1,000	100	2.5	20	0.5					
145	10700	1	83	30.07	45.5	100	45.5	1	1,000	10	10	1,000	100	2	20	0.4	2.77	2,313,820	988.76	18,124	99.22
150	11000	1	84	30.07	35	100	35	3	1,000	30	10	1,000	100	2.5	20	0.5	8.31	5,329,770	1783.85	98,094	98.16
155	11600	1	84	30.07	25	100	25	3	1,000	30	10	1,000	100	4	20	0.8	16.62	7,613,957	1579.40	86,851	98.86
160	12800	1.5	83	30.07	27	100	27	3	1,000	30	18	1,000	180	7	20	1.4	33.33	16,496,530	1932.66	106,277	99.36
165	13200	0.8	88	30.07	29	100	29	2	1,000	20	12	1,000	120	5	20	1	10.99	5,842,296	967.80	35,480	99.39
170	13200	0.5	97	30.07	36.5	100	36.5	0	1,000	0	1	1,000	10	2.5	20	0.5					
175	13200	0.5	101	30.07	35	100	35	0	1,000	0	0	1,000	0	2	20	0.4					
180	13800	0.5	89	30.07	28	100	28	4	1,000	40	5	1,000	50	4	20	0.8	16.44	8,439,661	1755.13	128,686	98.48
185	13800	0.5	92	30.07	40	100	40	3	1,000	30	8	1,000	80	4	20	0.8					
190	14500	0.6	90	30.07	47.5	100	47.5	3	1,000	30	14	1,000	140	6	20	1.2	19.15	16,677,197	2287.92	125,813	99.25
195	14800	1	89	30.07	45	100	45	3	1,000	30	13	1,000	130	6.5	20	1.3	8.23	6,790,152	860.15	47,300	99.30
200	14800	1	90	30.07	25	100	25	3	1,000	30	10	1,000	100	6	20	1.2					
205	15400	1	92	30.07	16	100	16	1	1,000	10	8	1,000	80	8	20	1.6	16.37	4,802,310	497.14	9,113	99.81
210	15800	0.5	99	30.07	10	100	10	2	1,000	20	2	1,000	20	5	20	1	10.77	1,973,496	330.26	12,107	99.39
215	15800	0.5	105	30.07	9	100	9	2	1,000	20	0.5	1,000	5	4.5	20	0.9					
220	15800	1	100	30.07	9	100	9	3	1,000	30	0	1,000	0	3	20	0.6					
225	16400	1	94	30.07	20	100	20	4	1,000	40	7	1,000	70	3.5	20	0.7	16.32	5,981,217	1420.79	104,172	98.26
230	17100	1	91	30.07	34	100	34	3	1,000	30	16	1,000	160	5	20	1	19.14	11,927,335	1961.91	107,885	99.10
235	17900	1	90	30.07	40	100	40	4	1,000	40	18	1,000	180	7.5	20	1.5	21.91	16,065,911	1752.96	128,527	99.20
240	18200	0.4	99	30.07	48	100	48	1	1,000	10	15	1,000	150	7	20	1.4	8.07	7,102,850	837.53	15,352	99.78
245	18200	0.4	100	30.07	47	100	47	0	1,000	0	0	1,000	0	11	20						
250	18200	0.3	100	30.07	45	100	45	0	1,000	0	0	1,000	0	10	20						

VRU EMISSION CALCULATIONS

COMPANY: COASTAL FUELS - PORT CANAVERAL
FACILITY: VAPOR COMBUSTION UNIT
DATE: 08/26/2003

	METER				INLET VOC, (AS PROPANE)			OUTLET VOC, (AS PROPANE)			CARBON MONOXIDE			CARBON DIOXIDE			INLET		OUTLET		FLARE
TIME	RDG.	STATIC	METER	BAROM.	ANALYZER	INSTRU.		ANALYZER	INSTRU.		ANALYZER	INSTRU.		ANALYZER	INSTRU.		GAS		GAS		CONTROL
(min)	cf	PRESSURE	TEMP.	PRESSURE	READING	SCALE	CONC.	READING	SCALE	CONC.	READING	SCALE	CONC.	READING	SCALE	CONC.	VOLUME	MASS	VOLUME	MASS	EFF.
	#1	("H2O)	(deg f)	("Hg)	(% CHART)	(%)	(%)	(% CHART)	(PPM)	(PPM)	(% CHART)	(PPM)	(PPM)	(% CHART)	(%)	(%)	(M3)*	(mg)	(M3)*	(mg)	(%)
255	18700	1	94	30.07	43	100	43	2	1,000	20	5	1,000	50	6	20	1.2	13.60	10,716,347	1485.10	54,444	99.49
260	19500	1	94	30.07	32	100	32	5	1,000	50	20	1,000	200	3	20	0.6	21.75	12,759,929	3451.85	316,362	97.52
265	20700	1.5	94	30.07	37.5	100	37.5	2	1,000	20	16	1,000	160	2	20	0.4	32.67	22,456,919	9376.11	343,728	98.47
270	21800	1	95	30.07	40	100	40	2.5	1,000	25	15	1,000	150	7	20	1.4	29.86	21,891,613	2573.01	117,908	99.46
275	21800	0.5	100	30.07	31	100	31	2.5	1,000	25	9	1,000	90	5	20	1					
280	22100	0.7	101	30.07	15	100	15	2	1,000	20	4	1,000	40	5	20	1	8.05	2,213,348	369.64	13,551	99.39
285	22500	0.4	103	30.07	10	100	10	1	1,000	10	3	1,000	30	7	20	1.4	10.69	1,958,996	233.01	4,271	99.78
290	22700	0.4	105	30.07	7.5	100	7.5	3	1,000	30	0.5	1,000	5	3	20	0.6	5.32	732,023	206.74	11,369	98.45
295	23100	0.6	107	30.07	8	100	8	3	1,000	30	0	1,000	0	6	20	1.2	10.62	1,556,901	216.13	11,885	99.24
300	23100	0	112	30.07	9	100	9	0	1,000	0	0	1,000	0	4	20	0.8					
305	23100	0	112	30.07	9	100	9	0	1,000	0	0	1,000	0	3	20	0.6					
310	23100	0.5	116	30.07	8.5	100	8.5	0	1,000	0	0	1,000	0	2	20	0.4					
315	23100	0	117	30.07	8	100	8	0	1,000	0	0	1,000	0	2	20	0.4					
320	23100	0	117	30.07	7.5	100	7.5	0	1,000	0	0	1,000	0		20	0					
325	23100	0	118	30.07	7.5	100	7.5	0	1,000	0	0	1,000	0	2	20	0.4					
330	23300	0.5	109	30.07	8	100	8	6	1,000	60	0.5	1,000	5	1	20	0.2	5.29	775,525	673.35	74,055	90.45
335	23400	0.5	108	30.07	10	100	10	4	1,000	40	2	1,000	20	5	20	1	2.65	485,556	80.76	5,921	98.78
340	24300	1	105	30.07	19	100	19	3	1,000	30	5	1,000	50	7	20	1.4	24.00	8,357,295	988.30	54,347	99.35
345	24700	1	105	30.07	20	100	20	4	1,000	40	10	1,000	100	5	20	1	10.67	3,909,846	645.07	47,297	98.79
350	24900	0.5	107	30.07	13	100	13	3	1,000	30	4	1,000	40	2	20	0.4	5.31	1,264,673	540.43	29,718	97.65
355	25600	0.5	107	30.07	20	100	20	2	1,000	20	4	1,000	40	3	20	0.6	18.58	6,809,779	1921.60	70,446	98.97
360	25600	0.5	107	30.07	25	100	25	2	1,000	20	4	1,000	40	4	20	0.8					
TOTAL	25600																705.166	364,003,677	76,040	3,469,155	
AVERAGE		0.7	90	30.06	25.6		26	2.2		22	6		63	4		0.8					98.48

* At standard conditions of 68 deg F and 29.92in. Hg)

EQUATIONS

VOLUME

$$V_{std} = (V_f - V_i) \times Y_m \times [P_{bar} + (P_g/13.6)]/P_{std} \times [T_{std}/T_m]$$

where:

V_{std} = Meter volume at standard conditions, $ft.^3$ at 528°Rankin and 29.92 in. Hg

Y_m = Meter correction factor

V_f = Final meter reading ($ft.^3$)

V_i = Initial meter reading ($ft.^3$)

P_{bar} = Barometric pressure (in. Hg)

P_g = Static pressure in duct (in. H_2O)

P_{std} = Standard pressure, 29.92 in. Hg

T_{std} = Absolute standard temperature, 528°Rankin

T_m = Absolute meter temperature (°Rankin)

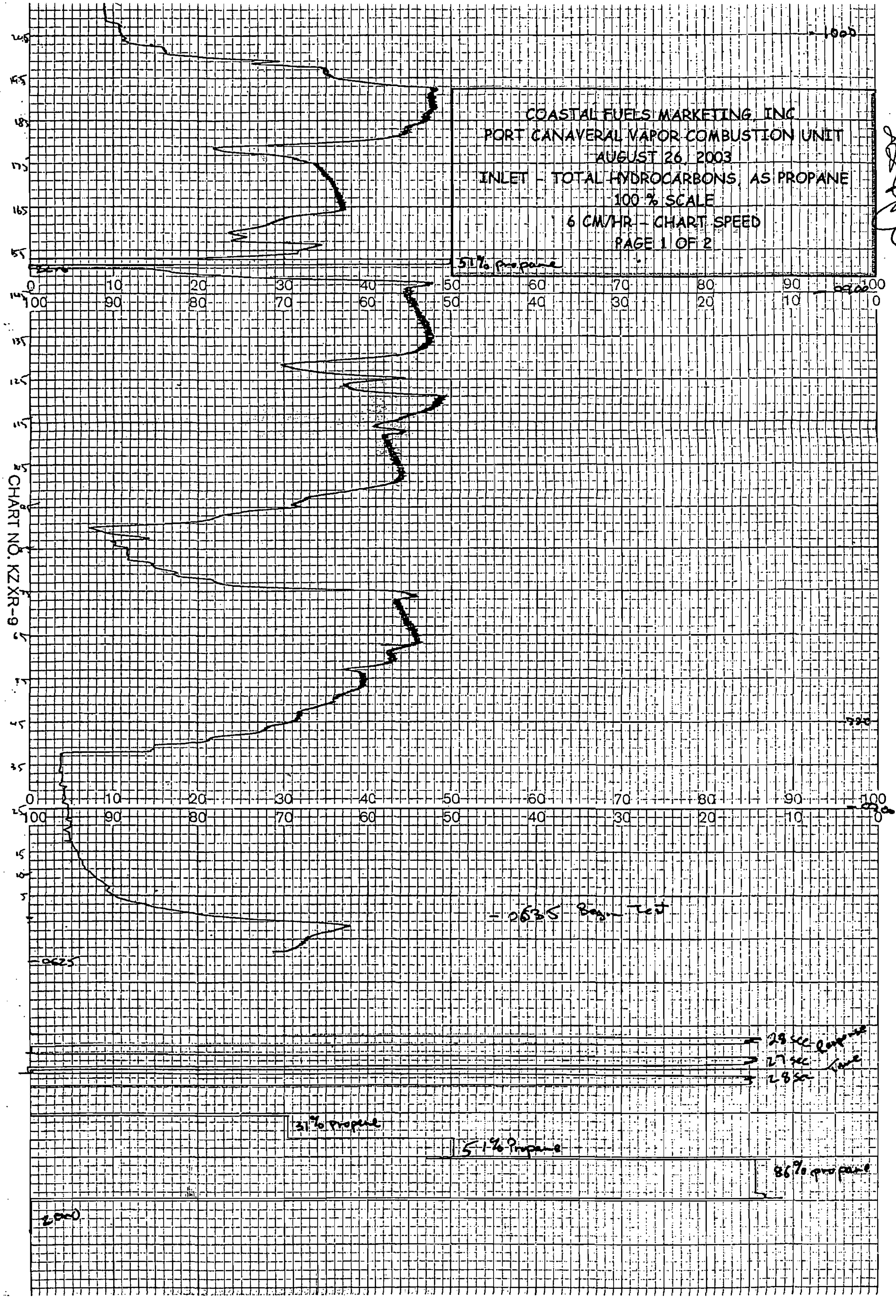
ORIFICE VELOCITY (5 MINUTE INTERVAL)

$$V_o = V_{std} / (A_o \times 5 \text{ min} \times 60 \text{ sec/min})$$

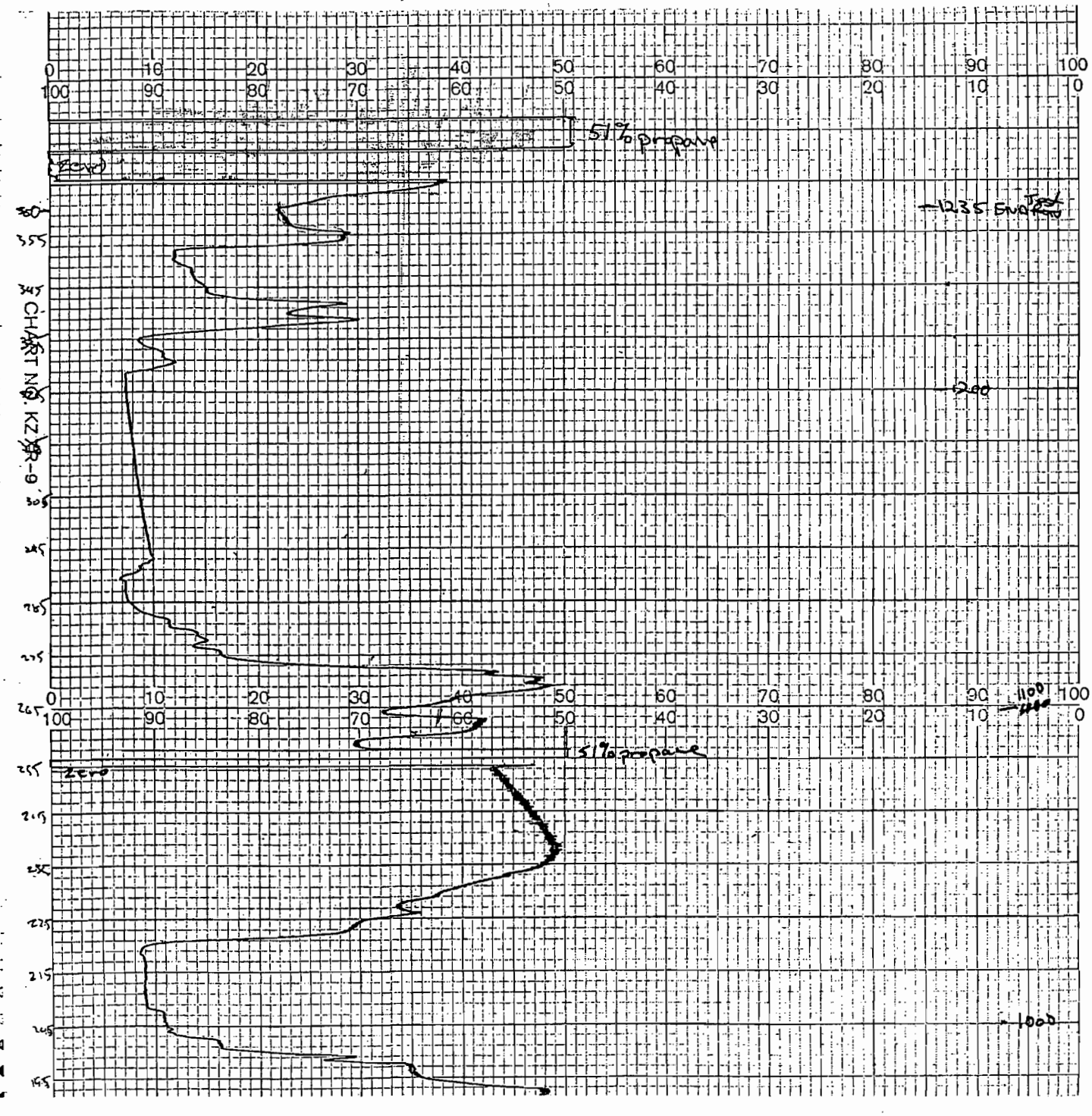
where:

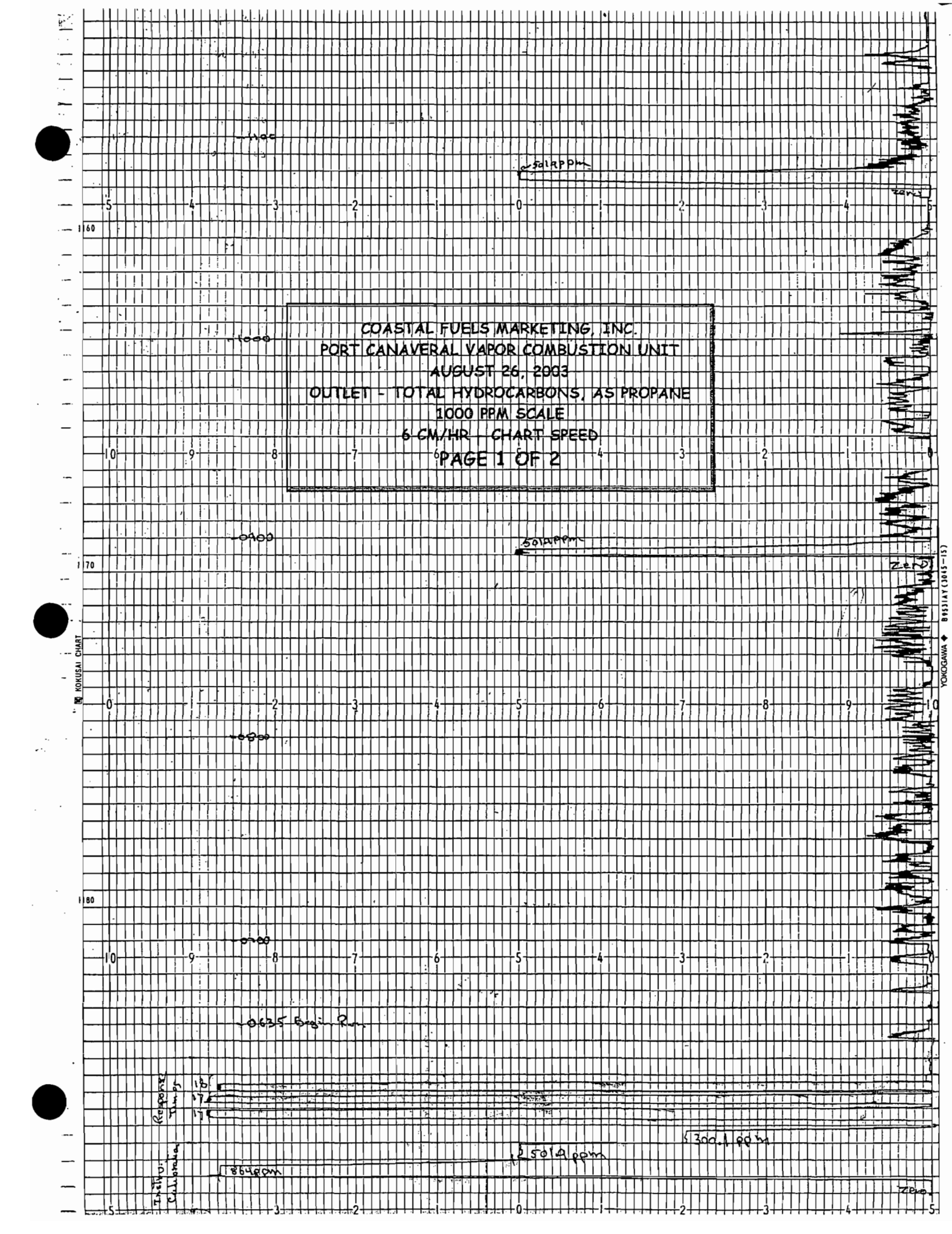
V_o = Velocity at flare burner orifice (ft./sec.)

A_o = Total area of orifice openings ($ft.^2$)

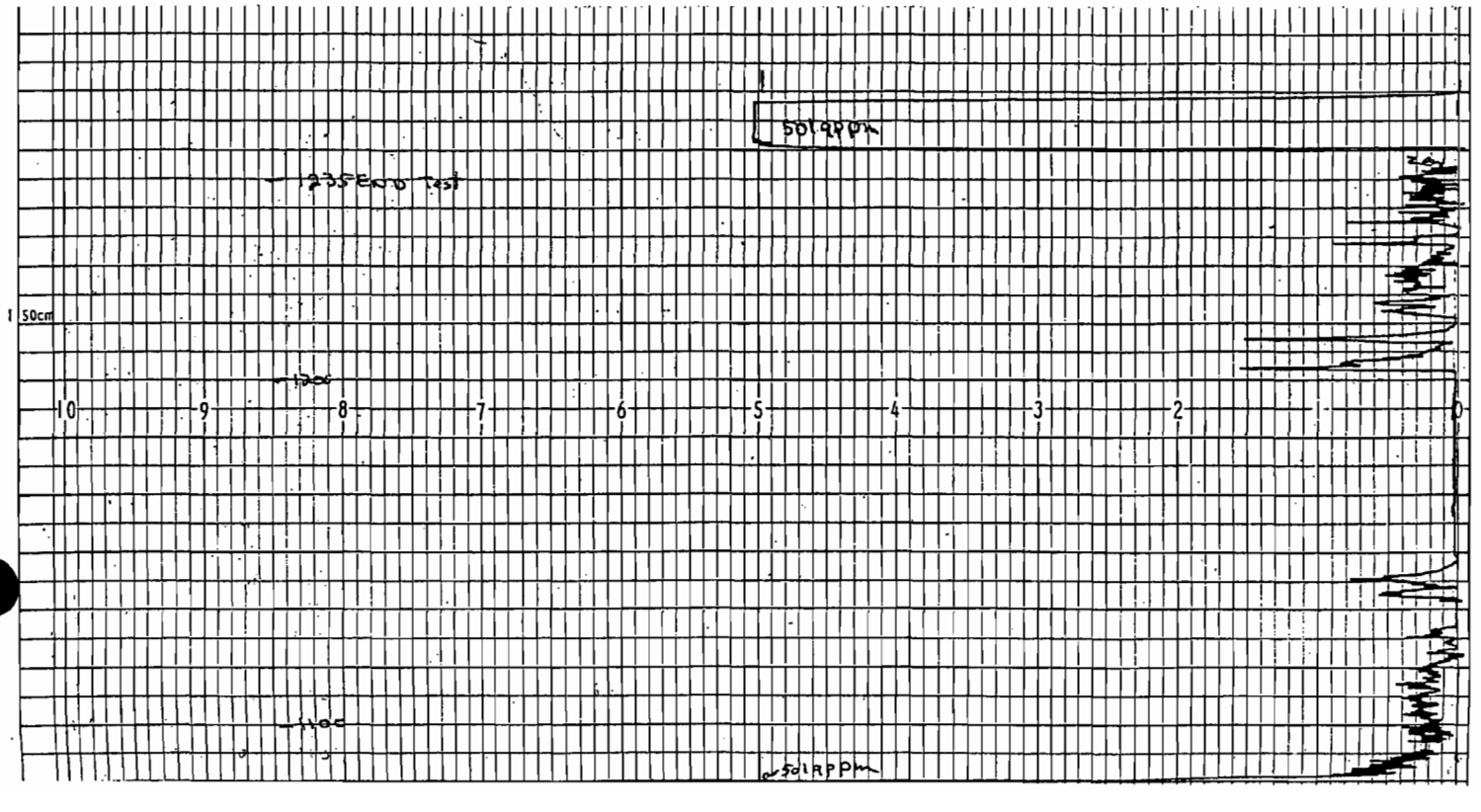

COASTAL FUELS MARKETING, INC
PORT CANAVERAL VAPOR COMBUSTION UNIT
AUGUST 26, 2003
INLET - TOTAL HYDROCARBONS, AS PROPANE
100 % SCALE
6 CM/HR - CHART SPEED
PAGE 1 OF 2
CHART NO. KZ XR-9
51% propane
- 1000
- 0900
- 0800
- 0635 Begin Test
- 0625
28 sec
27 sec
28 sec
31% propane
51% propane
86% propane

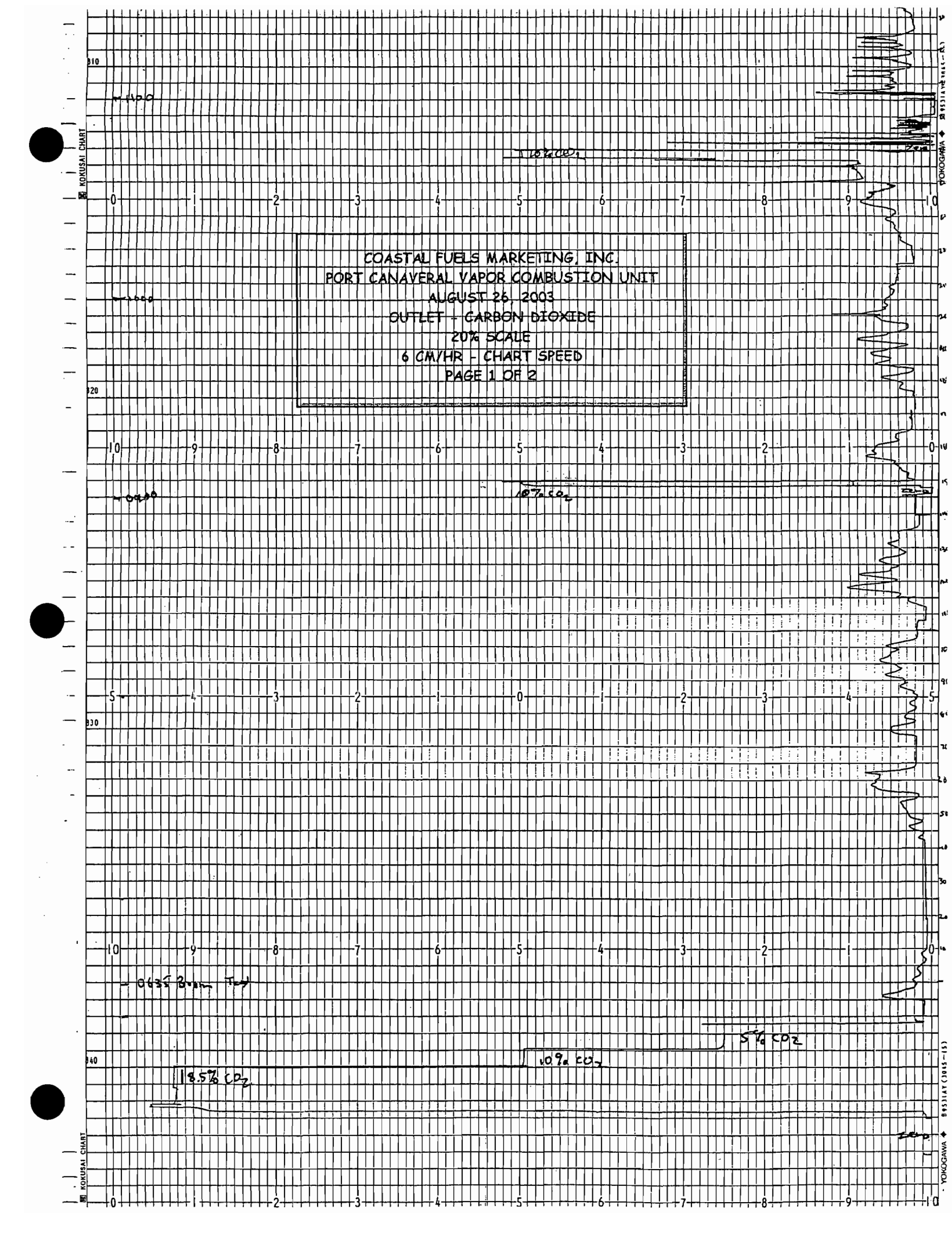
COASTAL FUELS MARKETING, INC.
PORT CANAVERAL VAPOR COMBUSTION UNIT
AUGUST 26, 2003
INLET - TOTAL HYDROCARBONS, AS PROPANE
100 % SCALE
6 CM/HR - CHART SPEED



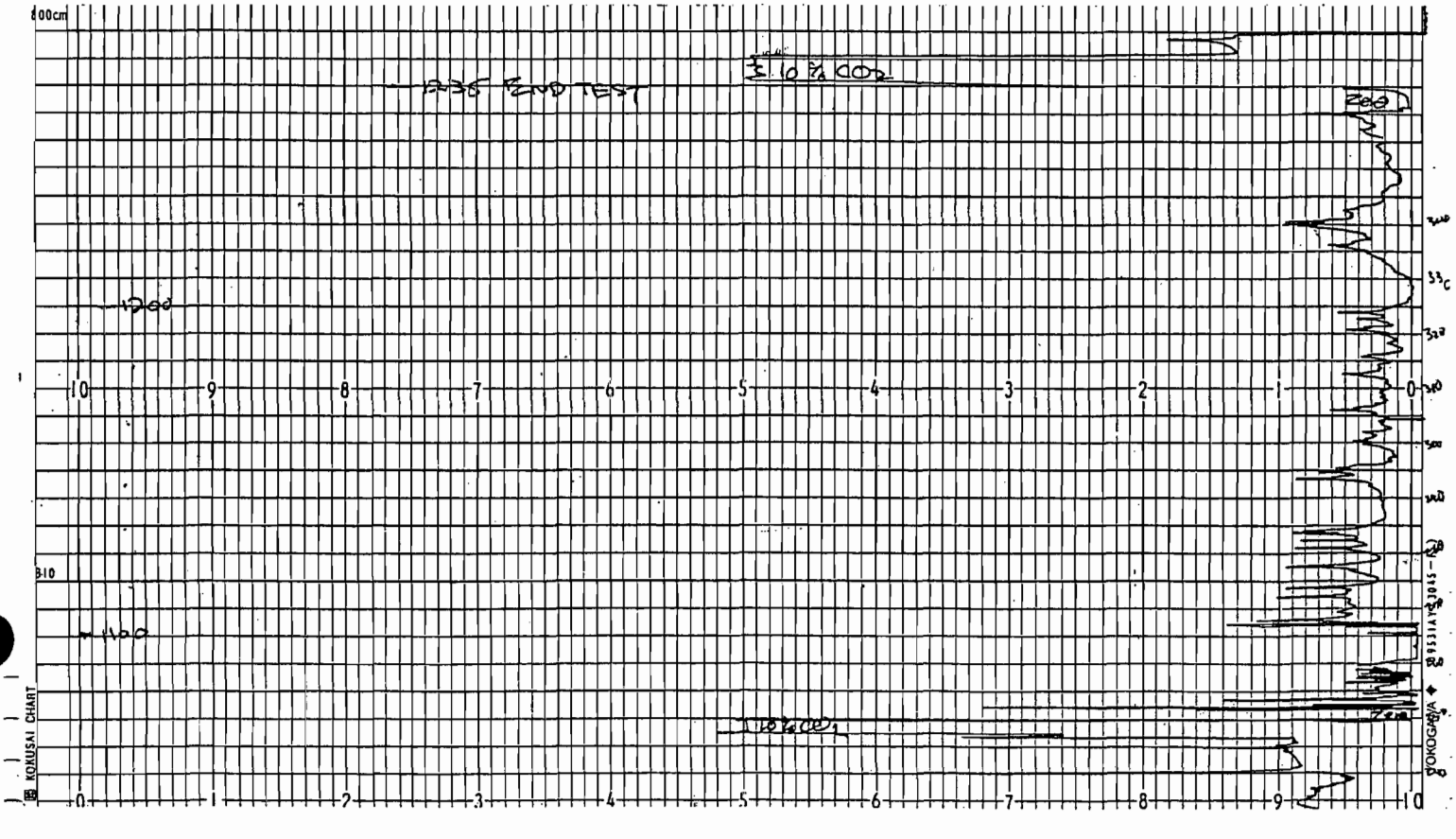

COASTAL FUELS MARKETING, INC.
PORT CANAVERAL VAPOR COMBUSTION UNIT
AUGUST 26, 2003
OUTLET - TOTAL HYDROCARBONS, AS PROPANE
1000 PPM SCALE
6 CM/HR - CHART SPEED
PAGE 1 OF 2
KOKUSAI CHART
YOKOGAWA

COASTAL FUELS MARKETING, INC.
PORT CANAVERAL VAPOR COMBUSTION UNIT
AUGUST 26, 2003
OUTLET - TOTAL HYDROCARBONS, AS PROPANE
1000 PPM SCALE
6 CM/HR - CHART SPEED
PAGE 2 OF 2

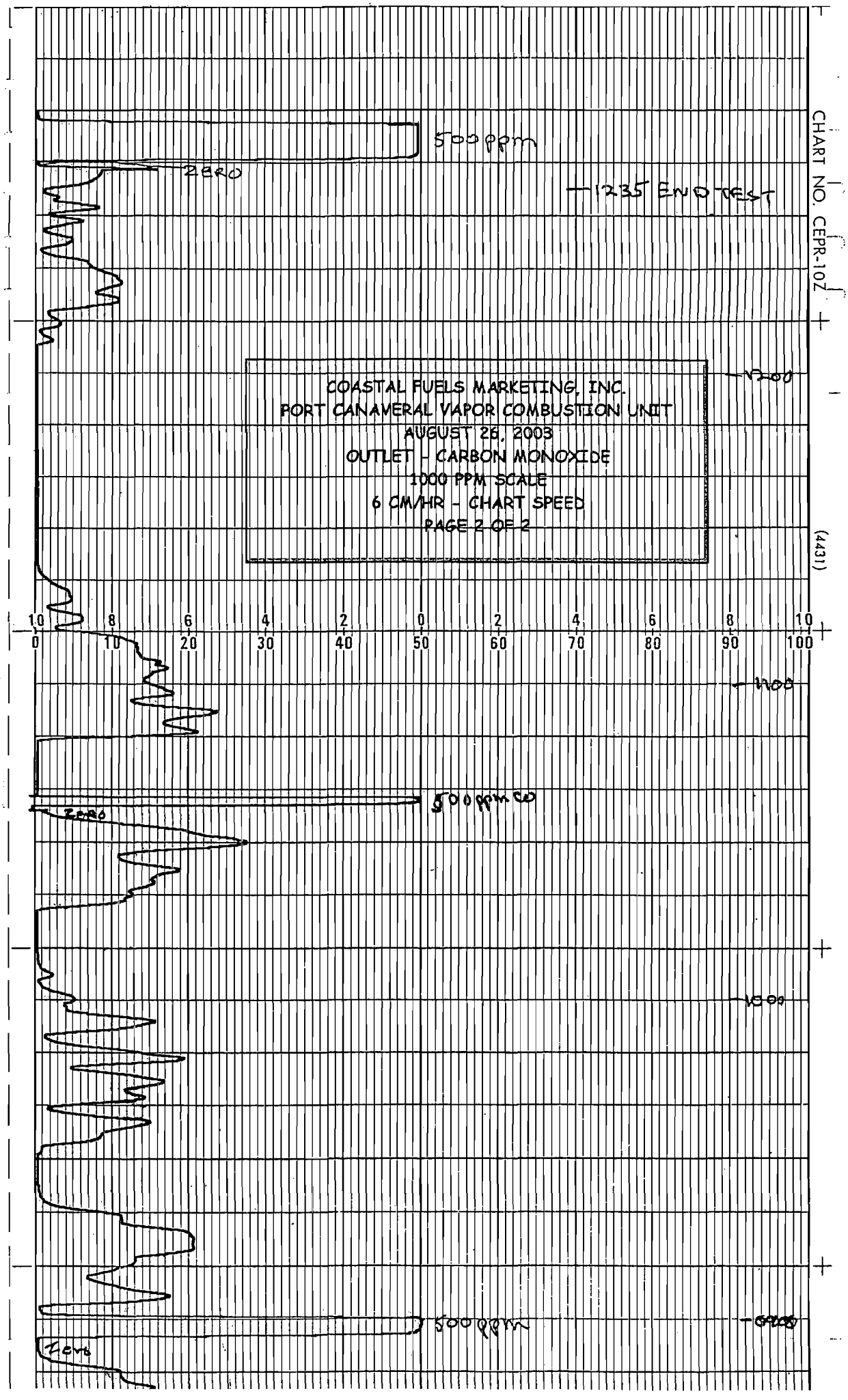



COASTAL FUELS MARKETING, INC.
PORT CANAVERAL VAPOR COMBUSTION UNIT
AUGUST 26, 2003
OUTLET - CARBON DIOXIDE
20% SCALE
6 CM/HR - CHART SPEED
PAGE 1 OF 2
KOKUSAI CHART
YOKOGAWA

COASTAL FUELS MARKETING, INC.
PORT CANAVERAL VAPOR COMBUSTION UNIT
AUGUST 26, 2003
OUTLET - CARBON DIOXIDE
20% SCALE
6 CM/HR - CHART SPEED
PAGE 2 OF 2



COASTAL FUELS MARKETING, INC.
PORT CANAVERAL VAPOR COMBUSTION UNIT
AUGUST 26, 2003
OUTLET - CARBON MONOXIDE
1000 PPM SCALE
6 CM/HR - CHART SPEED
PAGE 1 OF 2
500 ppm
Zero
250 ppm CO
500 ppm CO
902 ppm CO
Zero
0905
0800
0700
0635
0625
Charts Inc
CHART NO. CEPR-10Z
(4431)


500 ppm
ZERO
1235 END TEST
CHART NO. CEPR-10Z
COASTAL FUELS MARKETING, INC.
PORT CANAVERAL VAPOR COMBUSTION UNIT
AUGUST 26, 2003
OUTLET - CARBON MONOXIDE
1000 PPM SCALE
6 CM/HR - CHART SPEED
PAGE 2 OF 2
(4431)
10 8 6 4 2 0 2 4 6 8 10
0 10 20 30 40 50 60 70 80 90 100
500 ppm CO
ZERO
500 ppm

SOUTHERN ENVIRONMENTAL SCIENCES, INC.

GAS DILUTION SYSTEM FIELD EVALUATION

COMPANY	COASTAL FUELS MARKETING, INC.
SOURCE	PORT CANAVERAL VAPOR COMBUSTION UNIT
DATE	08/26/2003
DILUTION INSTRUMENT	ENVIRONICS MODEL 2020
SERIAL #	1899
MEASUREMENT INSTRUMENT	CALIFORNIA ANALYTICAL
SERIAL #	
SUPPLY GAS	8606 PPM

SUPPLY GAS (PPM)	MFM #	PREDICTED GAS CONC. (PPM)	INJECTION #1 (PPM)	#2 (PPM)	#3 (PPM)	AVERAGE (PPM)	ACCEPTABLE RANGE			% DIFFERENCE
8606	2	8100	8100	8050	8060	8070.0	8231.4	to	7908.6	-0.4%
8606	2	2500	2520	2520	2520	2520.0	2570.4	to	2469.6	0.8%
								to		
								to		
MID RANGE		5143	5100	5050	5100	5083.3	5185.0	to	4981.7	-1.2%

EPA METHOD 205 - VERIFICATION OF GAS DILUTION SYSTEMS FOR FIELD INSTRUMENT CALIBRATIONS
40 CFR 51, APPENDIX M

SOUTHERN ENVIRONMENTAL SCIENCES, INC.

1204 North Wheeler Street St. Plant City, Florida 33566 (813) 752-5014

METHOD 25A CALIBRATION

TEST DATA	
DATE	04/26/2003
COMPANY	COASTAL FUEL MARKETING, INC.
SOURCE	PORT CANAVERAL VAPOR COMBUSTION UNIT

INSTRUMENT DATA		
	MONITOR	RECORDER
MANUFACTURER	CALIF. ANAL.	YOKAGAWA
MODEL NO.	HID300(M)	302111
SERIAL NO.		
RANGE (%)	100	6 CM/HR

CALIBRATION GASES			
SUPPLIER	AIR PRODUCTS		
CYLINDER #	PROPANE		
CONCENTRATION	99.95		
EXPIRATION DATE			

CALIBRATION ERROR TEST (within 2 hrs. of test)									
Selected Range:	100	%							
Adjusted zero gas response:	0	%							
Adjusted span gas response:	86	%							
Linear Regression Analysis:	Slope:	1	Intercept:	0					
Mid-level gas response:	Predicted:	51	%	Actual:	50.3	%	% diff.	-1.4	
Low-level gas response:	Predicted:	31	%	Actual:	30.5	%	% diff.	-1.6	
RESPONSE TIME TEST									
1) 28 SECONDS			2) 27 SECONDS			3) 28 seconds			
TEST PERIOD									
Start Time: 0635						Stop Time: 1235			

DRIFT DETERMINATION					
	Zero			Span	
Time	Response (ppm)	% diff.(span)	Response (%)	Actual (%)	% diff (span)
0910	0	0	50	51	-2.0
1050	0	0	50.3	51	-1.4
1240	0	0	50.7	51	-0.6

SOUTHERN ENVIRONMENTAL SCIENCES, INC.

1204 North Wheeler Street St. Plant City, Florida 33566 (813) 752-5014

METHOD 25A CALIBRATION

TEST DATA	
DATE	08/26/2003
COMPANY	COASTAL FUELS MARKETING, INC.
SOURCE	PORT CANAVERAL VAPOR COMBUSTION UNIT

INSTRUMENT DATA		
	MONITOR	RECORDER
MANUFACTURER	CALIF. ANAL.	YOKOGAWA
MODEL NO.	HID300(M)	BD211
INSTR. NO.		
RANGE (PPM)	1,000	6 CM/HR

CALIBRATION GASES			
SUPPLIER	AIRGAS	AIRGAS	AIRGAS
CYLINDER #	SG91655331	SG9102825	SG896044
CONCENTRATION	864	501.9	300.1
EXPIRATION DATE	04/05/2006	07/07/2005	04/02/2006

CALIBRATION ERROR TEST (within 2 hrs. of test)								
Selected Range	1000	ppm						
Adjusted zero gas response	0	ppm						
Adjusted span gas response	864	ppm						
Linear Regression Analysis	Slope:	1	Intercept:	0				
Mid-level gas response	Predicted:	501.9	ppm	Actual:	498	ppm	% diff.	-0.8
Low-level gas response	Predicted:	300.1	ppm	Actual:	295	ppm	% diff.	-1.7

RESPONSE TIME TEST					
1)	17 SECONDS	2)	17 SECOND	3)	17 seconds

TEST PERIOD			
Start Time:	0635	Stop Time:	1235

DRIFT DETERMINATION					
	Zero			Span	
Time	Response (ppm)	% diff.(span)	Response (ppm)	Actual (ppm)	% diff.
0855	0	0	500	501.9	-0.4
1048	0	0	500	501.9	-0.4
1240	0	0	502	501.9	0.0

SOUTHERN ENVIRONMENTAL SCIENCES, INC.

1204 North Wheeler Street St. Plant City, Florida 33563 (813) 752-5014

INSTRUMENT CALIBRATION

TEST DATA	
DATE	08/26/2003
COMPANY	COASTAL FUELS MARKETING
SOURCE	PORT CANAVERAL VAPOR COMBUSTION UNIT
PARAMETER	**CARBON DIOXIDE**
TECHNICIAN	K. ROBERTS

INSTRUMENT DATA		
	MONITOR	RECORDER
MANUFACTURER	CALIF. ANAL.	YOKAGAWA
MODEL NO.	110	SINGLE PEN
SERIAL NO.		
RANGE (%)	20	6 CM/HR

CALIBRATION GASES			
SUPPLIER	Spectra Gases		
CYLINDER #	CC83934		
CONC. (%)	19.9		
EXPIRATION DATE	03/23/2004		

POINT	OBSERVED CONC.	ACTUAL CONC.	PERCENT DIFF.
1	0	0	0.00
2	5	5	0.00
3	9.9	10	-0.50
4	18.5	18.5	0.00

Regression Output:

Constant		-0.0177
Std Err of Y Est		0.0607
R Squared		1.0000
No. of Observations		4
Degrees of Freedom		2
X Coefficient(s)	0.9991	
Std Err of Coef.	0.0044	

SOUTHERN ENVIRONMENTAL SCIENCES, INC.

1204 North Wheeler Street St. Plant City, Florida 33566 (813) 752-5014

INSTRUMENT CALIBRATION

TEST DATA	
DATE	08/26/2003
COMPANY	COASTAL FUELS MARKETING
SOURCE	PORT CANAVERAL VAPOR COMBUSTION UNIT
PARAMETER	**CARBON MONOXIDE**
TECHNICIAN	K. ROBERTS

INSTRUMENT DATA		
	MONITOR	RECORDER
MANUFACTURER	TECO	METRONIC
MODEL NO.	48	
SERIAL NO.	48-27158-228	
RANGE (PPM)	1000	6CM/HR

CALIBRATION GASES			
SUPPLIER	SPECTRA GASES		
CYLINDER #	CC-126519		
CONC. (%)	902		
EXPIRATION DATE	07/03/2006		

POINT	OBSERVED CONC.	ACTUAL CONC.	PERCENT DIFF.
1	0	0	0.00
2	255	250	0.50
3	505	500	0.50
4	908	902	0.60

Regression Output:

Constant		1.6234
Std Err of Y Est		1.9109
R Squared		1.0000
No. of Observations		4
Degrees of Freedom		2
X Coefficient(s)	1.0058	
Std Err of Coef.	0.0029	

SOUTHERN ENVIRONMENTAL SCIENCES, INC.

PRESSURE MEASUREMENT DEVICE CALIBRATION FORM

Device Type	Magnehelic	Calibration Date	04/01/2003
Range	0 - 5" H2O	Calibrated by	K. Roberts
Manufacturer	Dwyer	Reference Device	Manometer
Serial No.	R890411RR3	Measurement Units	" H2O

Device Reading	Reference Device Reading	% Difference*
0.0	0.0	0.00
1	1	0.00
2.5	2.5	0.00
4.1	4	2.50
5.1	5	2.00

* % difference shall not exceed +/- 5%

SOUTHERN ENVIRONMENTAL SCIENCES, INC.

PRESSURE MEASUREMENT DEVICE CALIBRATION FORM

Device Type	Magnehelic	Calibration Date	04/01/2003
Range	0 - 20" H2O	Calibrated by	K. Roberts
Manufacturer	Dwyer	Reference Device	Manometer
Serial No.	R9602025L4	Measurement Units	" H2O

Device Reading	Reference Device Reading	% Difference*
0	0	0.00
5.1	5	2.00
10	10	0.00
15.3	15	2.00
19.9	20	-0.50

* % difference shall not exceed +/- 5%

SOUTHERN ENVIRONMENTAL SCIENCES, INC.

PRESSURE MEASUREMENT DEVICE CALIBRATION FORM

Device Type	Magnehelic	Calibration Date	04/01/2003
Range	0 - 20" H2O (M2)	Calibrated by	K. Roberts
Manufacturer	Dwyer	Reference Device	Manometer
Serial No.	R940629LPB12	Measurement Units	" H2O

Device Reading	Reference Device Reading	% Difference*
0	0	0.00
5	5	0.00
10.1	10	1.00
14.9	15	-0.67
20	20	0.00

* % difference shall not exceed +/- 5%

SOUTHERN ENVIRONMENTAL SCIENCES, INC.

PRESSURE MEASUREMENT DEVICE CALIBRATION FORM

Device Type	**Magnehelic**	**Calibration Date**	**04/01/2003**
Range	0 - 20" H2O (M3)	**Calibrated by**	K. Roberts
Manufacturer	Dwyer	**Reference Device**	Manometer
Serial No.	R940629LPD23	**Measurement Units**	" H2O

Device Reading	Reference Device Reading	% Difference*
0	0	0.00
5	5	0.00
10	10	0.00
15.2	15	1.33
19.6	20	-2.00

* % difference shall not exceed +/- 5%

SOUTHERN ENVIRONMENTAL SCIENCES, INC.
THERMOMETER CALIBRATIONS

Calibrated By/Date: T. Wilson 3/31/03

ALL TEMPERATURES ARE DEGREES RANKIN

ID No.	Type	Range	ICE BATH			TEPID WATER			BOILING WATER			HOT OIL		
			STD Therm	Temp	Deg or Diff	STD Therm	Temp	Deg or Diff	STD Therm	Temp	Deg or Diff	STD Therm	Temp	Deg or Diff
T1	PT	2000° F	495	496	0.2%	539	537	0.1%	672	670	0.2%	860	861	0.3%
T2	PT	2000° F	495	497	0.2%	539	537	0.1%	673	672	0.2%	870	872	0.3%
T3	PT	2000° F	495	497	0.2%	539	538	0.1%	673	671	0.3%	870	872	0.2%
T4	PT	2000° F	494	496	0.2%	539	538	0.1%	674	672	0.3%	863	864	0.2%
T5	PT	2000° F	494	496	0.2%	539	538	0.2%	672	670	0.2%	860	862	0.2%
T6	PT	2000° F	494	496	0.2%	539	537	0.3%	672	674	0.3%	852	854	0.2%
T7	PT	2000° F	495	497	0.2%	539	538	0.3%	673	671	0.2%	853	854	0.3%
T8	PT	2000° F	495	496	0.1%	539	537	0.2%	674	672	0.1%	864	865	0.2%
T9	PT	2000° F	495	497	0.1%	539	538	0.3%	673	671	0.1%	854	856	0.3%
Lab I4	BM	212° F	494	495	1°	536	535	1°	672	673	2°	-	-	-
I5	BM	250° F	494	495	1°	536	535	1°	672	672	2°	-	-	-
I6	BM	220° F	494	496	1°	536	536	2°	672	672	3°	-	-	-
SS110	BM	220° F	494	496	1°	540	539	2°	670	672	2°	-	-	-
SS300	PT	2000 °F	495	497	0.2%	540	538	0.1%	674	672	0.2%	850	852	0.2%
SS301	PT	2000° F	495	497	0.2%	540	538	0.2%	672	670	0.1%	856	858	0.2%
SS306	PT	2000° F	495	496	0.2%	540	538	0.2%	672	670	0.2%	856	858	0.2%
2.5'PA	PT	2000° F	495	496	0.2%	541	538	0.0%	673	672	0.2%	852	854	0.3%
2.5'PB	PT	2000° F	495	497	0.2%	541	538	0.0%	672	674	0.3%	856	858	0.3%
3'P	PT	2000° F	495	497	0.2%	541	539	0.1%	673	675	0.2%	858	860	0.3%
3'INC	PT	2000° F	494	496	0.1%	540	538	0.1%	676	678	0.2%	852	854	0.3%
5'PA	PT	2000° F	494	496	0.3%	540	539	0.0%	672	674	0.3%	856	858	0.2%
5'PB	PT	2000° F	495	497	0.3%	540	538	0.1%	674	672	0.3%	856	858	0.3%
5'PC	PT	2000° F	495	497	0.3%	540	538	0.2%	674	672	0.1%	856	858	0.3%
5'VP	PT	2000° F	495	497	0.2%	541	540	0.2%	676	678	0.2%	856	858	0.2%
5'INC	PT	2000° F	494	496	0.3%	542	540	0.1%	674	676	0.1%	850	852	0.3%
8'PA	PT	2000° F	494	496	0.3%	541	538	0.0%	676	678	0.2%	856	858	0.2%
8'PB	PT	2000° F	494	495	0.3%	541	539	0.1%	676	678	0.3%	856	858	0.2%
10'P	PT	2000° F	494	495	0.2%	541	539	0.0%	674	676	0.3%	854	856	0.2%

Quality Control Limits: Impinger Thermometers± 2°F, Bimetalic Thermometers(Bm)± 5°F,Pyrometers/Thermocouples(PT)± 1.5%

Southern Environmental Sciences, Inc.

1204 North Wheeler Street Plant City, Florida 33566 (813)752-5014

COMBUSTIBLE GAS DETECTOR CALIBRATION

INSTRUMENT

Manufacturer	GasTech
Model No.	GT105
Serial No.	9708311

CALIBRATION GAS DATA

	Zero	Span
Gas Type	Zero Air	methane
Concentration (PPM)	0	25,370
Supplier	Airgas	Air Products

CALIBRATION

	Observed Conc. (PPM)	Actual Conc. (PPM)	Percent Diff.
ZERO	0	0	0
SPAN	50% LEL	50% LEL	0
Response Time	6		
Calibration Date	8/26/03	Signature: Ken Rabert	

Note: For methane 10,000 PPM = 20% LEL

Southern Environmental Sciences, Inc.

1204 North Wheeler Street Plant City, Florida 33566 (813)752-5014

COMBUSTIBLE GAS DETECTOR CALIBRATION

INSTRUMENT

Manufacturer	Gastech
Model No.	GT.105
Serial No.	9709402

CALIBRATION GAS DATA

	Zero	Span
Gas Type	Zero Air	Methane
Concentration (PPM)	0	25,370
Supplier	AirGas	Air Products

CALIBRATION

	Observed Conc. (PPM)	Actual Conc. (PPM)	Percent Diff.
ZERO	0	0	0
SPAN	50% LEL	50% LEL	0
Response Time	5.5		
Calibration Date	8/26/03	Signature: Ken Roberts	

Note: For methane 10,000 PPM = 20% LEL

Southern Environmental Sciences, Inc.
1204 North Wheeler Street Plant City, Florida 33566 (813) 752-5014

TURBINE METER CALIBRATION

Turbine Meter No	94-54464
Pipot Cp	0.99
Calibration Date	04/25/2003
Serial No.	B. Nelson

		Run 1	Run 2	Run 3
Delta P Readings ("H2O)	P1	0.03	0.03	0.03
	P2	0.03	0.03	0.02
	P3	0.03	0.03	0.03
	P4	0.03	0.03	0.03
	P5	0.03	0.02	0.03
	P6	0.03	0.03	0.03
	P7	0.02	0.02	0.02
	P8	0.02	0.03	0.03
Avg. Sq. Rt of Delta P ("H2O)		0.1653	0.1653	0.1653
Temp. Readings (Deg F)	T1	74	75	74
	T2	74	75	75
	T3	74	75	75
	T4	74	75	75
	T5	74	75	75
	T6	74	75	76
	T7	74	75	76
	T8	75	75	75
Avg. Temperature		74.125	75.0	75.1
Static Pressure ("H2O)		0.68	0.65	0.64
Barometric Pressure ("Hg)		30.02	30.02	30.02
Moisture (%)		2.0	2.0	2.0
Total Pressure ("Hg)		30.07	30.07	30.07
Molecular Weight		28.54	28.54	28.54
Duct Diameter (inches)		12	12	12
Duct Area (sq. ft)		0.7854	0.7854	0.7854
Duct Velocity (ft/min)		11.04	11.05	11.05
Reference Flowrate (ACFM)		520.4	520.9	520.9
Test Meter Flowrate (ACFM)		530	530	530
Difference (%)		1.8	1.7	1.7

Average Difference (%)	1.75
Tolerance (%)	5

Airgas

Airgas Specialty Gases
5480 Hamilton Blvd.
Theodore, AL 36582

P.O. Box 190969
Mobile, AL 36619
(251) 653-2500 Fax (251) 653-2530
http://www.airgas.com

Certificate of Analysis: E.P.A. Protocol Gas Mixture

Cylinder No :	SG896044	Order No.	110586109
Cylinder Pressure:	2000 PSI	Expiration Date:	4/3/06
Certification Date	4/3/03	Laboratory:	ASG-MOBILE
Part Number:	E02NI99E15A0681		

Reference Standard Information:

Type	Component	Cyl. Number	Concentration
NTRM 81669	PROPANE	CC45854	476 ppm

Instrumentation:

Instrument/Model/Serial No.	Analytical Principle
SIEMENS FIDAMAT 5E-P, K4-391	FID

Analytical Methodology does not require correction for analytical interferences.

Certified Concentrations:

Component	Concentration	Accuracy	Procedure
PROPANE	300.1 PPM	+/-1%	G1
NITROGEN	Balance		

Analytical Results:

1st Component: PROPANE

1st Analysis Date: 3/31/03

R	476.0	S	300.1	Z	0.0	Conc	300.1 ppm
S	300.1	Z	0.0	R	476.0	Conc	300.1 ppm
Z	0.0	R	476.0	S	300.1	Conc	300.1 ppm
						AVG:	300.1 ppm

Certification performed in accordance with "EPA Traceability Protocol (Sept. 1997)" using the assay procedures listed.

Do not use cylinder below 150 psig.

Approved for Release

Airgas

Airgas Specialty Gases
12722 S. Wentworth Avenue
Chicago, IL 60628
773-785-3000 Fax: 773-785-1928
www.airgas.com

Certificate of Analysis: E.P.A. Protocol Gas Mixture

Certification performed in accordance with "EPA Traceability Protocol (Sept.1997)" using assay procedures listed.

Cylinder No:	SG9102825ALB	Order No:	904484-00
Certification Date:	07/8/2002	Expiration Date:	07/8/2005
Cylinder Pressure:	2000	Part No:	E02NI99E15A0932

*Do not use cylinder below 150 psig.

Component	*Certified Concentration*	*Unit of Measure*	*Accuracy*	*Procedure*	*Analytical Principle*
Propane	501.9	ppm	1%	G-1	FID
Nitrogen	Balance				
Nox (Reference Value Only)		ppm			

Reference Standard Information

Type	*Component*	*Concentration*	*Unit*	*Cylinder Number*
Ntrm	Propane	483.6	ppm	SG9101963ALB

Analytical Data

Component 1 Propane

1st Analysis Date: 07/8/2002

Zero	0.000	Cand	935289.000	Ref	899770.000
Zero	0.000	Cand	935014.000	Ref	901572.000
Zero	0.000	Cand	936014.000	Ref	900623.000

2nd Analysis Date:

Zero		Cand		Ref	
Zero		Cand		Ref	
Zero		Cand		Ref	

Approved by:

For Technical Information Call
1-800-752-1597

AIR PRODUCTS

Air Products and Chemicals, Inc. * 12722 S. Wentworth Avenue, Chicago, IL 60628

ISO CERTIFICATION: 9002

CERTIFICATE OF ANALYSIS: EPA PROTOCOL GAS STANDARD

PERFORMED ACCORDING TO EPA TRACEABILITY PROTOCOL FOR ASSAY AND CERTIFICATION OF GASEOUS CALIBRATION STANDARDS (PROCEDURE #G1)

Customer: 851 -1
APCI-LARGO
7900 118TH AVENUE NORTH
LARGO FL 33773-

Order No: CSS697640-01
Batch No: 86181394
PO:
Release:

Cylinder No: SG9165531BAL
Bar Code No: FDM902
Cylinder Pressure*: 2000 psig
Certification Date: 04/06/2001
Expiration Date: 04/06/2004

CERTIFIED CONCENTRATION		REFERENCE STANDARDS			ANALYTICAL INSTRUMENTATION			
Component	Certified Concentration	Cylinder Number	Standard Type	Standard Concentration	Instrument Make/Model	Serial Number	Last Calibration	Measurement Principal
PROPANE	864±5.5 PPM	SG9128533BAL	GMIS	1026 PPM	Gow-Mac 750	59405U	04/02/01	GC-FID

NITROGEN Balance Gas

*** STANDARD SHOULD NOT BE USED BELOW 150 PSIG**

EPA PROTOCOL GAS MIXTURE : PROPANE IN NITROGEN
To reorder this mixture please use Mix ID: 29928

Analyst: HOLLY HATTENDORF

Approved By: James Laas

(16921)

Pub. No. 320-9702

SPECTRA GASES INC.
3434 Route 22 West • Branchburg, NJ 08876 USA Tel.: (908) 252-9300 • (800) 932-0624 • Fax: (908) 252-0811
Shipped From: 80 Industrial Drive • Alpha, NJ 08865 www.spectra-gases.com

CERTIFICATE OF ANALYSIS

EPA PROTOCOL MIXTURE
PROCEDURE # : G1

CUSTOMER:	Cherokee Instruments Inc.	CYLINDER # :	CC-126519
SGI ORDER # :	0038770	CYLINDER PRES:	2000 PSIG
ITEM# :	18	CGA OUTLET:	350
P.O.# :	5609		

CERTIFICATION DATE: 7/3/2003
EXPIRATION DATE: 7/3/2006

CERTIFICATION HISTORY

COMPONENT	DATE OF ASSAY	MEAN CONCENTRATION	CERTIFIED CONCENTRATION	ANALYTICAL ACCURACY
Carbon Monoxide	6/24/2003 7/3/2003	903.6 ppm 901.2 ppm	902 ppm	+/- 1%

BALANCE Nitrogen

PREVIOUS CERTIFICATION DATES: None

REFERENCE STANDARDS

COMPONENT	SRM/NTRM#	CYLINDER#	CONCENTRATION
Carbon Monoxide	NTRM-81681	CC-55793	994 ppm

INSTRUMENTATION

COMPONENT	MAKE/MODEL	SERIAL #	DETECTOR	CALIBRATION DATE(S)
Carbon Monoxide	Horiba VIA-510	570423011	NDIR	6/24/2003

THIS STANDARD IS NIST TRACEABLE. IT WAS CERTIFIED ACCORDING TO THE EPA PROTOCOL PROCEDURES.
DO NOT USE THIS STANDARD IF THE CYLINDER PRESSURE IS LESS THAN 150 PSIG.

ANALYST: Cheryl L Patino
CHERYL PATINO

DATE: 7/3/2003

SPECTRA GASES INC.
3434 South 22 West • Bridgeburg, NJ 08276 USA Tel: (856) 252-9300 • (800) 932-0624 • Fax: (856) 252-0811
Shipped from: 80 Industrial Drive • Alpha, NJ 08865

CERTIFICATE OF ANALYSIS

EPA PROTOCOL MIXTURE

PROCEDURE #: G1

CUSTOMER: Cherokee Instruments Inc.
SGI ORDER #: 0003039
ITEM#: 11
P.O.#: 4060

CYLINDER #: CC83934
CYLINDER PRES: 2000 PSIG
CGA OUTLET: 590

CERTIFICATION DATE: 3/23/2001
EXPIRATION DATE: 3/23/2004

CERTIFICATION HISTORY

COMPONENT	DATE OF ASSAY	MEAN CONCENTRATION	CERTIFIED CONCENTRATION	ANALYTICAL ACCURACY
Carbon Dioxide	3/23/2001	19.90 %	19.90 %	+/- 1%
Oxygen	3/23/2001	19.83 %	19.83 %	+/- 1%

BALANCE: Nitrogen

PREVIOUS CERTIFICATION DATES: None

REFERENCE STANDARDS

COMPONENT	SRM/NTRM#	CYLINDER#	CONCENTRATION
Carbon Dioxide	NTRM-82745x	CC709414	20.00 %
Oxygen	NTRM-82659x	CC83908	22.8 %

INSTRUMENTATION

COMPONENT	MAKE/MODEL	SERIAL #	DETECTOR	CALIBRATION DATE(S)
Carbon Dioxide	Horiba VIA-510	571417UH5	NDIR	3/20/2001
Oxygen	Horiba MPA-510	570534U21	PM	3/20/2001

THIS STANDARD IS NIST TRACEABLE. IT WAS CERTIFIED ACCORDING TO THE EPA PROTOCOL PROCEDURES.
DO NOT USE THIS STANDARD IF THE CYLINDER PRESSURE IS LESS THAN 150 PSIG.

ANALYST: FRED PIKULA

DATE: 3/23/2001

BOILER ROLLING 12 MONTH RECORDS

PART II

Coastal Fuels Marketing, Inc. - Cape Canaveral Terminal

Air Permit # 0090029-003-AV

COPY

		Boiler 1				Boiler 2			
		Type of Fuel	Avg. Sulfur Content %	Total Hours	Fuel Vol. (gals or therms)	Type of Fuel	Avg. Sulfur Content %	Total Hours	Fuel Vol. (gals or therms)
31-Jan	**2003**	-	-	0	0	-	-	0.0	0.0
28-Feb	2003	-	-	0	0	RDSL		165.7	2,293.3
31-Mar	2003	-	-	0	0	-	-	0.0	0.0
30-Apr	2003	-	-	0	0	RDSL		46.1	629.0
31-May	2003	-	-	0	0	RDSL		32.0	553.7
30-Jun	2003	-	-	0	0	RDSL		71.9	1,148.3
31-Jul	2003	-	-	0	0	RDSL		46.8	884.5
31-Aug	2003	-	-	0	0	-	-	0	0
September	2003								
October	2003								
November	2003								
December	2003								
January	**2004**								
February	2004								
March	2004								
April	2004								
May	2004								
June	2004								
July	2004								
August	2004								
September	2004								
October	2004								
November	2004								
December	2004								

Note: Natural Gas Meter Units are in Therms

BOILER ROLLING 12 MONTH RECORDS

Coastal Fuels Marketing, Inc. - Cape Canaveral Terminal

Air Permit # 0090029-003-AV

Note: Natural Gas Meter Units are in Therms

		Boiler 1				Boiler 2			
		Type of Fuel	Avg. Sulfur Content %	Total Hours	Fuel Vol. (gals or therms)	Type of Fuel	Avg. Sulfur Content %	Total Hours	Fuel Vol. (gals or therms)
31-Jan	**2001**	RDSL	0.039	87	1,914	-	-	0	0
28-Feb	2001	RDSL	0.044	7.3	933.63	-	-	0	0
31-Mar	2001	RDSL	0.032	27.5	290.4	-	-	0	0
30-Apr	2001	RDSL		70.7	575.63	-	-	0	0
31-May	2001	RDSL	0.0444	55.3	590	-	-	0	0
30-Jun	2001	-	-	0	0	-	-	0	0
31-Jul	2001	RDSL	<0.05%	40.4	343.5	-	-	0	0
31-Aug	2001	-	-	0	0	-	-	0	0
30-Sep	2001	RDSL	<0.05%	100.8	1421	-	-	0	0
31-Oct	2001	RDSL	<0.05%	47.7	702	-	-	0	0
30-Nov	2001	-	-	0	0	-	-	0	0
31-Dec	2001	RDSL	<0.05%	2.9	55	-	-	0	0
31-Jan	**2002**	RDSL	<0.05%	78.1	1104	-	-	0	0
28-Feb	2002	RDSL	<0.05%	95.2	1449.5	-	-	0	0
31-Mar	2002	RDSL	<0.05%	5.8	113.5	-	-	0	0
30-Apr	2002	-	-	0	0	-	-	0	0
31-May	2002	RDSL	0.0418	55.2	789.55	-	-	0	0
30-Jun	2002	-	-	0	0	-	-	0	0
31-Jul	2002	-	-	0	0	-	-	0	0
31-Aug	2002	-	-	0	0	-	-	0	0
30-Sep	2002	RDSL	0.041	7.6	9.007368	RDSL	0.041	3.2	3.792576
31-Oct	2002	-	-	0	0	RDSL	0.041	50.2	990.449
30-Nov	2002	-	-	0	0	-	-	0	0
31-Dec	2002	-	-	0	0	RDSL	0.0395	80.25	428.6

COPY

HEATER ROLLING 12 MONTH RECORDS
PART II
Coastal Fuels Marketing, Inc. - Cape Canaveral Terminal
Air Permit #0090029-003AV

		Heater 6				
		Type of Fuel	Avg. Sulfur Content %	Total Hrs	Fuel Vol. Gals	Fuel Vol. Therms
31-Jan	**2003**	Nat Gas	-	537.82	-	33,035.59
28-Feb	2003	Nat Gas	-	306.90	-	16,910.00
31-Mar	2003	Nat Gas	-	566.85		32,350.00
30-Apr	2003	Nat Gas	-	560.60	-	31,143.57
31-May	2003	-	-	-	-	-
30-Jun	2003	-	-	-	-	-
31-Jul	2003	-	-	-	-	-
31-Aug	2003	-	-	-	-	-
September	2003					
October	2003					
November	2003					
December	2003					
January	**2004**					
February	2004					
March	2004					
April	2004					
May	2004					
June	2004					
July	2004					
August	2004					
September	2004					
October	2004					
November	2004					
December	2004					

RDSL = Low Sulfur Diesel

HEATER ROLLING 12 MONTH RECORDS

Coastal Fuels Marketing, Inc. - Cape Canaveral Terminal

Air Permit #0090029-003AV

Note: Natural Gas Meter Units are in Therms

		Heater 6				
		Type of Fuel	Avg. Sulfur Content %	Total Hrs	Fuel Vol. Gals	Fuel Vol. Therms
31-Jan	**2001**	RDSL	0.035	206.1	8,118	-
		Nat. Gas	-	0.25	-	1.07
28-Feb	2001	-	-	0	0	0.00
		-	-	0	0	0.00
31-Mar	2001	RDSL	0.032	1.1	11.6	-
		Nat. Gas	-	40.5	-	176.59
30-Apr	2001	-	-	0	0	0.00
31-May	2001	-	-	0	0	0.00
30-Jun	2001	-	-	0	0	0.00
31-Jul	2001	-	-	0	0	0.00
31-Aug	2001	-	-	0	0	0.00
30-Sep	2001	Nat. Gas	-	5.6	-	32.48
31-Oct	2001	Nat. Gas	-	347.89	-	1,978.40
30-Nov	2001	-	-	0	0	0.00
31-Dec	2001	-	-	0	0	0.00
31-Jan	**2002**	-	-	0	0	0.00
28-Feb	2002	-	-	0	0	0.00
31-Mar	2002	Nat. Gas	-	88.13	-	479.87
30-Apr	2002	-	-	0	0	0
31-May	2002	-	-	0	0	0.00
		Nat. Gas	-	35.72	-	180.09
30-Jun	2002	-	-	0	-	0.00
31-Jul	2002	Nat. Gas	-	56.28		289.24
31-Aug	2002	Nat. Gas	-	374.66		2,228.47
30-Sep	2002	-	-	0	0	-
		Nat Gas	-	474.2	-	2,813.19
31-Oct	2002	-	-	0	0	0
		-	-	0	0	0
30-Nov	2002	Nat Gas	-	582.2	-	3,909.00
31-Dec	2002	Nat Gas	-	555.92	-	3,677.18

HEATER ROLLING 12 MONTH RECORDS

Coastal Fuels Marketing, Inc. - Cape Canaveral Terminal

Air Permit #0090029-003AV

Note: Natural Gas Meter Units are in Therms
RDSL = Low Sulfur Diesel

COPY

HEATER ROLLING 12 MONTH RECORDS
PART II
Coastal Fuels Marketing, Inc. - Cape Canaveral Terminal
Air Permit #0090029-003AV

		Heater 5				
		Type of Fuel	Avg. Sulfur Content %	Total Hrs	Fuel Vol. Gals	Fuel Vol. Therms
31-Jan	**2003**	Nat Gas	-	33.12	-	2,034.40
28-Feb	2003	-	-	0.00	-	-
31-Mar	2003	-	-	0.00	-	-
30-Apr	2003	Nat Gas	-	65.10	-	3,616.57
31-May	2003	Nat Gas	-	499.34	-	34,540.00
30-Jun	2003	Nat Gas	-	525.30	-	35,660.00
31-Jul	2003	Nat Gas	-	604.10	-	38,710.00
31-Aug	2003	Nat Gas	-	536.33	-	31,710.00
September	2003					
October	2003					
November	2003					
December	2003					
January	**2004**					
February	2004					
March	2004					
April	2004					
May	2004					
June	2004					
July	2004					
August	2004					
September	2004					
October	2004					
November	2004					
December	2004					

RDSL = Low Sulfur Diesel

HEATER ROLLING 12 MONTH RECORDS

Coastal Fuels Marketing, Inc. - Cape Canaveral Terminal

Air Permit #0090029-003AV

Note: Natural Gas Meter Units are in Therms

		Heater 5				
		Type of Fuel	Avg. Sulfur Content %	Total Hrs	Fuel Vol. Gals	Fuel Vol. Therms
31-Jan	**2001**	RDSL -	0.039 -	543.2 -	21,395.8 -	- -
28-Feb	2001	RDSL Nat Gas	0.088 -	123.6 543.6	5,026 -	- 3,889.00
31-Mar	2001	RDSL Nat Gas	0.032 -	1.0 726.8	10.56 -	- 4,345.41
30-Apr	2001	Nat Gas	-	715.7	-	4,431.00
31-May	2001	Nat Gas	-	735.1	-	4,508.00
30-Jun	2001	Nat Gas	-	613.8	-	3,525.00
31-Jul	2001	Nat Gas	-	684.2	-	3,798.00
31-Aug	2001	Nat Gas	-	702.6	-	4,090.00
30-Sep	2001	Nat Gas	-	659.7	-	3,826.26
31-Oct	2001	Nat Gas	-	388.3	-	2,338.60
30-Nov	2001	Nat Gas	-	707.7	-	4,312.00
31-Dec	2001	Nat Gas	-	736.2	-	4,922.00
31-Jan	**2002**	Nat Gas	-	662.9	-	3,990.00
28-Feb	2002	Nat Gas	-	662.9	-	3,724.00
31-Mar	2002	Nat Gas	-	732.81	-	3,990.15
30-Apr	2002	Nat Gas	-	710.9	-	4,293.00
31-May	2002	RDSL Nat Gas	0.0382 -	51 676.16	2568.2 -	- 3,408.91
30-Jun	2002	Nat Gas	-	694.71	-	3,409.00
31-Jul	2002	Nat Gas	-	739.15	-	3,798.76
31-Aug	2002	Nat Gas	-	307.42		1,828.53
30-Sep	2002	RDSL Nat Gas	0.041 -	38.9 111.7	1164.5 -	- 662.66
31-Oct	2002	RDSL Nat Gas	0.041 -	54.3 560.28	- -	1,520.10 3,416.50
30-Nov	2002	Nat Gas	-	60.15	-	406.50
31-Dec	2002	Nat Gas	-	80.25	-	530.82

HEATER ROLLING 12 MONTH RECORDS

Coastal Fuels Marketing, Inc. - Cape Canaveral Terminal

Air Permit #0090029-003AV

Note: Natural Gas Meter Units are in Therms
RDSL = Low Sulfur Diesel

Clean Air Consulting, Inc.
18218 N. 30th. St., Lutz, FL 33559
Phone: (813) 948-6025 Fax: (813) 949-0659

COPY

June 10, 2002

Mr. Leonard T. Kozlov
Department of Environmental Protection
Division of Air Resources Management
3319 Maguire Boulevard, Suite 232
Orlando, Florida 32803-3767

RE: COASTAL FUELS MARKETING, INC. - CAPE CANAVERAL
PERMIT NO. 0090029-003-AV

Dear Mr. Kozlov:

The annual visible emission test was conducted on the Boiler No. 1 at the Cape Canaveral Terminal on May 1, 2002.

The tests were conducted by Jim Estler of Clean Air Consulting, Inc. and a copy of the VE report and fuel analysis is attached.

Hot Oil Heaters Nos. 4 & 5 have been fired primarily on natural gas during the past 12 months. No. 2 fuel oil was used less than 400 hours per year per heater. Therefore, visible emission testing is not required on these units pursuant to Rule 62-297.310(7)(a)5, F.A.C. Boiler No. 2 is not operational at this time.

If you have any questions regarding this matter, please give me a call.

Sincerely,

James Wm. Estler, Q.E.P.
President

Encl:

cc: Rex Thompson with attachments
Dan Tibbits with attachments
Rich Vogel with attachments ✓

VISIBLE EMISSION OBSERVATION

Method Used: Method 9 | Other:

Company Name: Coastal Fuels Marketing, Inc
Facility Name: Cape Canaveral Terminal
Street Address: 8592 N. Atlantic Ave
City: Cape Canaveral | State: FL | Zip: 32920

Process: Boiler | Unit #: 1 | Operating Mode: to high fire
Control Equipment: NA | Operating Mode: NA

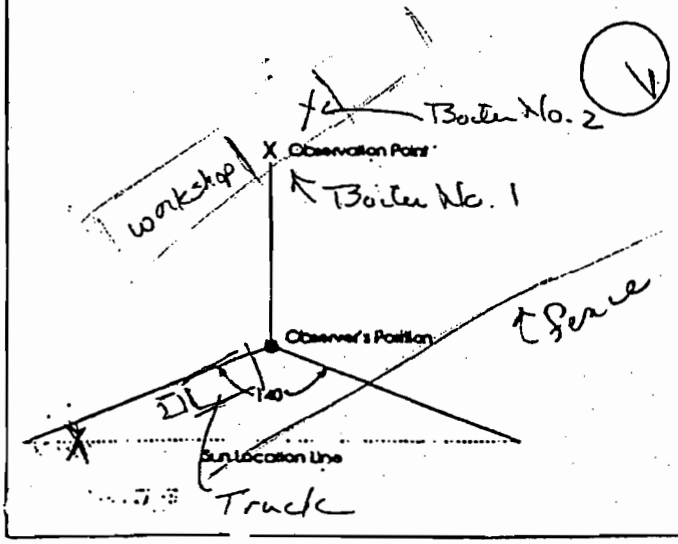
Describe Emission Point: Stack with rain cap
Height of Emiss. Pt.: ~17ft | Height of Emiss. Pt. Rel. to Observer: ~14ft
Distance to Emiss. Pt.: ~60ft | Direction to Emiss. Pt. (Degrees): SW ~215-220°

Permit No. 0090029-003-AV
Emissions Unit 001

Describe Emissions: None observed
Emission Color: NA | Water Droplet Plume: Attached ☐ Detached ☐ None ☒

Describe Plume Background: Sky / tank
Background Color: blue/green | Sky Conditions: clear
Wind Speed: ~2-5 mph | Wind Direction: ~west
Ambient Temp.: ~85°F

Source Layout Sketch — Draw North Arrow



Additional Information: Fired on No. 2 fuel oil; Sulfur Content = 0.0382%

Observation Date: 5/1/02 | Start Time: 11:05AM | End Time: 11:35AM

Sec / Min	0	15	30	45	Comments
1	0	0	0	0	Boiler cycled to
2	0	0	0	0	high fire from cold
3	0	0	0	0	start - steam vented
4	0	0	0	0	to maintain high
5	0	0	0	0	fire (~11.9gal/hr)
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	
25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

Observer's Name (Print): Jim Esther
Observer's Signature: [signature] | Date: 5/1/02
Organization: Clean Air Consulting, Inc
Certified By: FDEP | Date: Feb 2002

VISIBLE EMISSION OBSERVATION

Method Used: Method 9 | Other: _____

Company Name: Coastal Fuels Marketing, Inc
Facility Name: ~~Tanker Terminal~~ Cape Canaveral
Street Address: 8952 N. Atlantic Ave
City: Cape Canaveral | State: FL | Zip: 32920

Process: Boiler | Unit #: 1 | Operating Mode: High fire
Control Equipment: NA | Operating Mode: NA

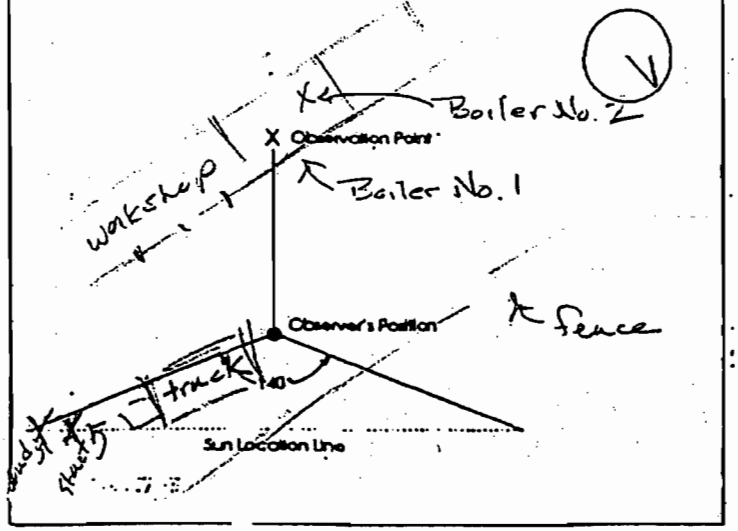
Describe Emission Point: Stack w/ rain cap
Height of Emiss. Pt.: ~12ft | Height of Emiss. Pt. Rel. to Observer: ~14ft
Distance to Emiss. Pt.: ~60ft | Direction to Emiss. Pt. (Degrees): SW ~215°-220°

Perm.# No. 0090029-003-AV
Emission Unit 001

Describe Emissions: Puffs
Emission Color: grey | Water Droplet Plume: Attached ☐ Detached ☐ None ☒

Describe Plume Background: Sky / tank
Background Color: Blue / green | Sky Conditions: Clear
Wind Speed: ~2-5 mph | Wind Direction: ~ West, South west.
Ambient Temp.: ~80°F

Source Layout Sketch — Draw North Arrow



Additional Information:

Observation Date: 5/1/02 | Start Time: 11:35AM | End Time: 12:05PM

Sec / Min	0	15	30	45	Comments
1	0	0	0	0	
2	0	0	0	0	
3	0	0	0	0	
4	5	5	0	0	max. 6 minute
5	0	0	0	0	Overage = 0.4 %
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	
25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	5	5	0	
30	0	0	0	0	

Observer's Name (Print): Jim Estler
Observer's Signature: [signature] | Date: 5/1/02
Organization: Clean Air Consulting, Inc
Certified By: FDEP | Date: Feb. 2002

COPY

Clean Air Consulting, Inc.
18218 N. 30th. St., Lutz, FL 33559
Phone: (813) 948-6025 Fax: (813) 949-0659

May 22, 2003

Mr. Leonard T. Kozlov
Department of Environmental Protection
Division of Air Resources Management
3319 Maguire Boulevard, Suite 232
Orlando, Florida 32803-3767

RE: COASTAL FUELS MARKETING, INC. - CAPE CANAVERAL
PERMIT NO. 0090029-003-AV

Dear Mr. Kozlov:

The annual visible emission test was conducted on the Boiler No. 2 at the Cape Canaveral Terminal on May 6, 2003.

The test was conducted by Jim Estler of Clean Air Consulting, Inc. A copy of the VE report and fuel analysis is attached.

Boiler No. 1 is not operational and therefore was not tested. The two hot oil heaters were fired primarily on natural gas during the past 12 months. No. 2 fuel oil was used less than 400 hours per year per heater. Therefore, visible emission testing was not required on these units pursuant to Rule 62-297.310(7)(a)5, F.A.C.

If you have any questions regarding this matter, please give me a call.

Sincerely,

James Wm. Estler, Q.E.P.
President

Encl:

cc: Rex Thompson with attachments
Rich Vogel with attachments

VISIBLE EMISSION OBSERVATION

Method Used: Method 9 | Other: _____

Company Name: Coastal Fuels Marketing, Inc.
Facility Name: Cape Canaveral Terminal
Street Address: 8592 N. Atlantic Ave
City: Cape Canaveral | State: FL | Zip: 32920

Process: Boiler No. 2 | Unit: N/A | Operating Mode: to high fire
Control Equipment: NA | Operating Mode: NA

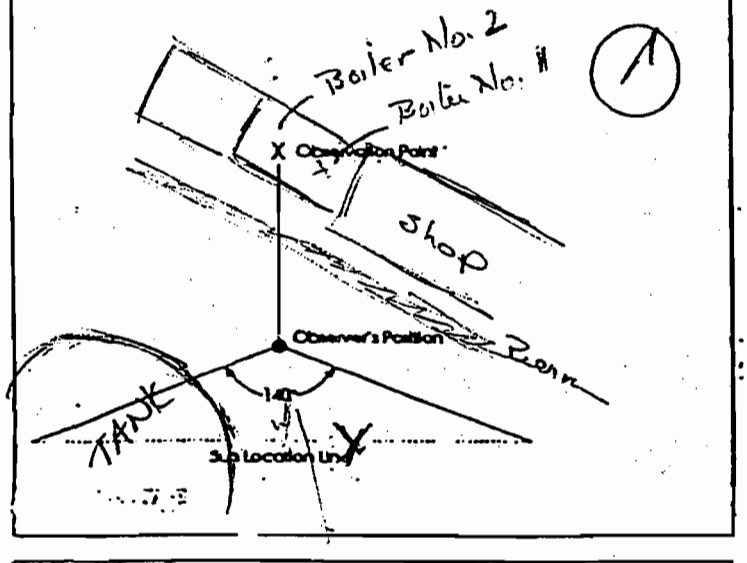
Describe Emission Point: stack w/ rain cap
Height of Emiss. Pt.: ~14 ft | Height of Emiss. Pt. Rel. to Observer: ~12 ft
Distance to Emiss. Pt.: ~80 ft | Direction to Emiss. Pt. (Degrees): 335° NW

Fired on No. 2 Fuel Oil
FDEP Permit No.: 0090029-003-AV
Emission Unit No.: 002

Describe Emissions: lite gray puff
Emission Color: lite gray | Water Droplet Plume: Attached ☐ Detached ☐ None ☒

Describe Plume Background: sky
Background Color: white / blue | Sky Conditions: layer of thin high clouds
Wind Speed: ~5-8 mph | Wind Direction: E
Ambient Temp.: ~86°F | ~63% R.H.

Source Layout Sketch — Draw North Arrow



Observation Date: 5/6/03 | Start Time: 10:52 AM | End Time: 11:22 AM

Sec / Min	0	15	30	45	Comments
1	0	0	0	0	
2	0	0	0	0	
3	0	0	0	0	
4	0	0	0	0	
5	0	0	0	0	
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	5	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	
25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

Additional Information:
Boiler cycled to high fire from cold start...
steam vented to maintain high fire ~19 gal/hr

Observer's Name (Print): Tim Estler
Observer's Signature: [signature] | Date: 5/6/03
Organization: Clean Air Consulting, Inc
Certified By: FDEP | Date: Feb. 2003

VISIBLE EMISSION OBSERVATION

Method Used: (Method 9) Other: _____

Company Name: Coastal Fuels Marketing, Inc.
Facility Name: Cape Canaveral Terminal
Street Address: 8592 N. Atlantic Ave
City: Cape Canaveral | State: FL | Zip: 32920

Process: Boiler No. 2 | Unit #: 2 | Operating Mode: 70 high fire
Control Equipment: NA | Operating Mode: NA

Describe Emission Point: stack w/ rain cap
Height of Emiss. Pt.: ~14 ft | Height of Emiss. Pt. Rel. to Observer: ~12 ft
Distance to Emiss. Pt.: ~80 ft | Direction to Emiss. Pt. (Degrees): 335° N

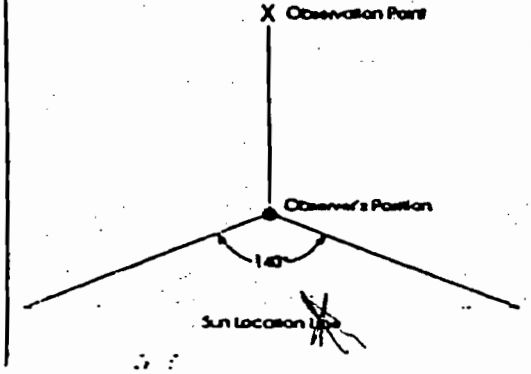
Fired on No. 2 Fuel Oil
FDEP Permit No.: 0090029-003-AV

Describe Emissions: lite gray puff
Emission Color: lite gray | Water Droplet Plume: Attached ☐ Detached ☐ None ☒

Describe Plume Background: sky
Background Color: white/blue | Sky Conditions: Layer of high thin clouds
Wind Speed: ~5-8 mph | Wind Direction: E
Ambient Temp.: ~86 °F to 87 °F | ~63% R.H. to 71% RH

Source Layout Sketch — Draw North Arrow

See page 1 of 2 for details



Additional Information:

Observation Date: 5/6/03 | Start Time: 11:22 AM | End Time: 11:52 AM

Sec / Min	0	15	30	45	Comments
1	0	0	0	0	
2	0	0	0	0	
3	0	0	0	0	
4	0	0	0	0	
5	0	0	0	0	
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	
25	0	0	0	0	MAX. six minute average = 0.6%
26	10	5	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

Observer's Name (Print): Jim Estler
Observer's Signature: [signature] | Date: 5/6/03
Organization: Clean Air Consulting, Inc.
Certified By: FDEP | Date: Feb. 2002

ITS Intertek Testing Services
Caleb Brett

12. QUALITY INFORMATION

LOW SULPHUR DIESEL(CPL-74 with exceptions)

REPORT OF ANALYSIS

Samples Drawn By: ITS Caleb Brett Inspector
Analysis Carried Out By: Coastal Personnel in their terminal
Analysis Attented By: ITS Caleb Brett Lab Technician
Analysis Performed From/To: February 20-21, 2003

TEST	*UNIT*	*METHOD*	*RESULT*	
			Sb.Tk. 911	Vsl Comp
API Gravity @ 60F		ASTM D1298	36.7	36.2
Haze Rating @ 77F		ASTM D4176	#1	#1
Apperance	None	ASTM D4176	Clear/Bright	Clear/Bright
Color, ASTM	None	ASTM D1500	<1.0	<1.0
Sulphur	Wt %	ASTM D4294	0.038	0.044
Flash Point (PMCC)	Deg F	ASTM D93	194	198
Viscosity @ 100F	Cst	ASTM D445	3.28	3.45
Cloud Point	Deg F	ASTM D2500	10	12
Pour Point	Deg F	ASTM D97	0	0
Copper Corrosion (3Hrs @ 122F)		ASTM D130	#1	#1
Cetane Index		ASTM D976	52.3	52.1
BS & W	Vol %	ASTM D2709	0.005	0.005
Rams.Bt.Carb.Resd.-10% BTM	Wt %	ASTM D524	0.07	0.07
Ash	Wt %	ASTM D482	0.0009	0.0009
Thermal Stability-90min. @ 150 C	PAD #	DUPONT SCALE	#1	#1
Distillation	Deg F	ASTM D86		
		IBP	410	425
		50 % Recovered	532	539
		90 % Recovered	601	606
		End Point	644	643

For ITS Caleb Brett Aruba

The reported analysis was performed by Coastal Refinery Laboratory personnel and witnessed by Intertek Testing Services Caleb Brett. Our responsibility is solely to witness that the analysis is conducted on the correct sample(s). Customer agrees that Intertek Testing Services Caleb Brett is not responsible for the condition of apparatus, instrumentation and measuring devices, and that Intertek Testing Services / Caleb Brett accepts calibration data, reagents, solutions, etc. as presented.

COPY

Clean Air Consulting, Inc.
18218 N. 30th. St., Lutz, FL 33549
Phone: (813) 948-6025 Fax: (813) 949-0659

Post-it Fax Note	Date 4/27/01	# of pages 8
To Rich Vogel		
Fax# Cape VE Test Report		
From Jim Estler		
Phone#		

April 25, 2001

Mr. Leonard T. Kozlov
Department of Environmental Protection
Division of Air Resources Management
3319 Maguire Boulevard, Suite 232
Orlando, Florida 32803-3767

RE: COASTAL FUELS MARKETING, INC. - CAPE CANAVERAL
PERMIT NO. 0090029-003-AV

Dear Mr. Kozlov:

or 5% per permit

The annual visible emission tests were conducted on the Boiler No. 1 and Oil Heaters Nos. 4 & 5 at the Cape Canaveral Terminal on March 30, 2001. Boiler No. 2 is not operational at this time.

The tests were conducted by Jim Estler of Clean Air Consulting, Inc. and a copy of the VE reports and fuel analysis is attached.

If you have any questions regarding this matter, please give me a call.

Sincerely,

James Wm. Estler, Q.E.P.
President

cc: Craig Smith with attachment
Dan Tibbits with attachment

VISIBLE EMISSION OBSERVATION

Boiler No. 1 Page 1 of 2

Method Used: Method 9 Other: _____

Company Name: Coastal Fuels Marketing
Facility Name: Cape Canaveral
Street Address: 8954 N. Atlantic Ave
City: Cape Canaveral State: FL Zip: 32920

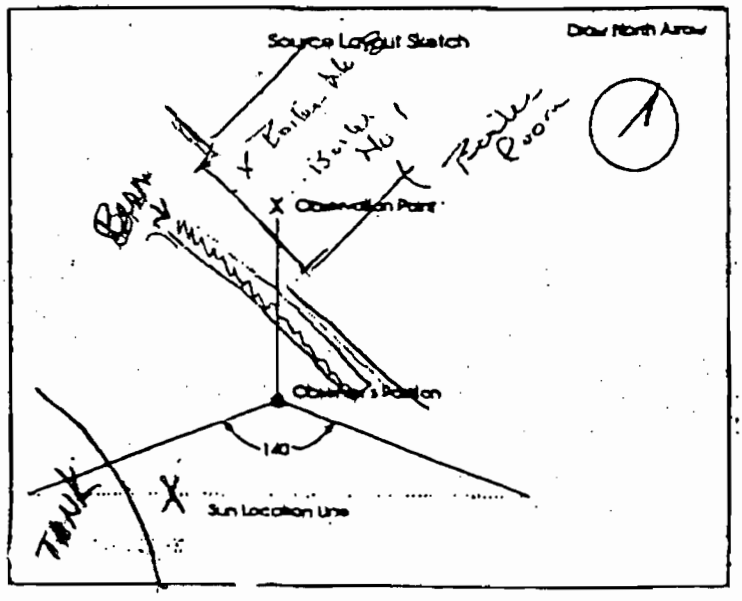
Process: Boiler Unit #: 1 Operating Mode: High Fire
Control Equipment: NA Operating Mode: NA

Describe Emission Point: stack w/ rain cap.
Height of Emiss. Pt.: ~145ft Height of Emiss. Pt. Rel. to Observer: ~125ft
Distance to Emiss. Pt.: ~80ft Direction to Emiss. Pt. (Degrees): NW 320°

Describe Emissions: None Observed
Emission Color: NA Water Droplet Plume: Attached ☐ Detached ☐ None ☒

Describe Plume Background: Sky
Background Color: Grey/White Sky Conditions: Partly cloudy
Wind Speed: 5-15 mph Wind Direction: South
Ambient Temp.: ~75°F

Source Layout Sketch — Draw North Arrow



Observation Date	Start Time	End Time
3/30/01	1:00 PM	1:30 PM

Sec / Min	0	15	30	45	Comments
1	0	0	0	0	
2	0	0	0	0	
3	0	0	0	0	
4	0	0	0	0	
5	0	0	0	0	
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	
25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

Observer's Name (Print): Jim Estler
Observer's Signature: _____ Date: 3/30/01
Organization: Clean Air Consulting, Inc
Certified by: FDEP Date: Feb. 2001

Additional Information:
Boiler cycled to high fire from cold start
Steam vent to maintain high fire
Fired on No. 2 fuel oil (~14 gal/hr)

VISIBLE EMISSION OBSERVATION

Boiler No. 1 Page 2 of 2

Method 9 / Other

Company Name: Coastal Fuels Marketing
Facility Name: Cape Canaveral
Street Address: 8954 N. Atlantic Ave
City: Cape Canaveral | State: FL | Zip: 32920

Process: Boiler | Unit #: 1 | Operating Mode: High Fire
Control Equipment: NA | Operating Mode: NA

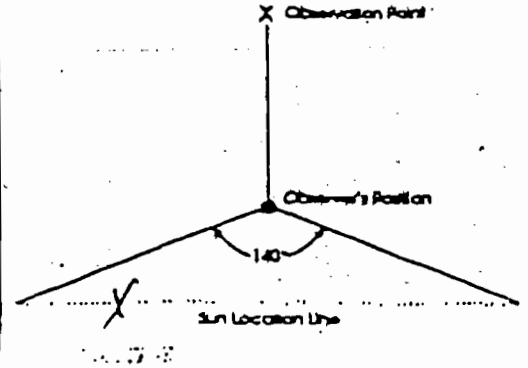
Describe Emission Point: stack w/ rain cap
Height of Emiss. Pt.: ~14ft | Height of Emiss. Pt. Rel. to Observer: ~12ft
Distance to Emiss. Pt.: ~80ft | Direction to Emiss. Pt. (Degrees): NW 320°

Describe Emissions: None Observed
Emission Color: NA | Water Droplet Plume: Attached ☐ Detached ☐ None ☒

Describe Plume Background: sky
Background Color: Grey/White | Sky Conditions: overcast
Wind Speed: 5-15 mph | Wind Direction: South
Ambient Temp.: ~75°F

Source Layout Sketch — Draw North Arrow

See page one for diagram
Observer location did not change



Additional Information:

Observation Date: 3/30/01 | Start Time: 1:30 PM | End Time: 2:00 PM

Sec / Min	0	15	30	45	Comments
1	0	0	0	0	
2	0	0	0	0	
3	0	0	0	0	
4	0	0	0	0	
5	0	0	0	0	
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	
25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

Observer's Name (Print): Jim Estler
Observer's Signature: [signature] | Date: 3/30/01
Organization: Clean Air Consulting, Inc
Certified By: FDEP | Date: Feb. 2001

Heater No. 4 Page 1 of 2

VISIBLE EMISSION OBSERVATION

Method 9 / Other: _____

Company Name: Coastal Fuels Marketing
Facility Name: Cape Canaveral
Street Address: 8954 N. Atlantic Ave
City: Cape Canaveral | State: FL | Zip: 32920

Process: Heater | Unit #: 4 | Operating Mode: High fire
Control Equipment: NA | Operating Mode: NA

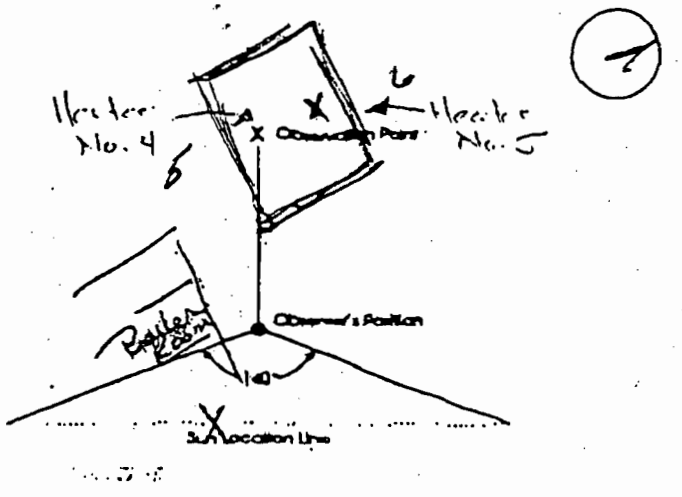
Describe Emission Point: stack w/ rain cap

Height of Emiss. Pt.: ~30ft | Height of Emiss. Pt. Rel. to Observer: ~27ft
Distance to Emiss. Pt.: ~80 ft | Direction to Emiss. Pt. (Degrees): 296° W

Describe Emissions: None Observed.
Emission Color: NA | Water Droplet Plume: Attached ☐ Detached ☐ None ☒

Describe Plume Background: sky
Background Color: white/gray | Sky Conditions: cloudy
Wind Speed: calm/light 7-10 | Wind Direction: South
Ambient Temp.: ~68°F

Source Layout Sketch — Draw North Arrow



Additional Information: Heater taken to high fire on No. 2.
Fuel Oil (~60 gal/hr)

Observation Date: 3/30/01 | Start Time: 10:46AM | End Time: 11:15AM

Sec / Min	0	15	30	45	Comments
1	0	0	0	0	
2	0	0	0	0	
3	0	0	0	0	
4	0	0	0	0	
5	0	0	0	0	
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	
25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

Observer's Name (Print): Jim Esther
Observer's Signature: [signature] | Date: 3/30/01
Organization: Clean Air Consulting INC
Certified By: FDEP | Date: Feb. 2001

Heater No. 4 Page 2 of 2

VISIBLE EMISSION OBSERVATION

Reference Used: Method 9 Other: _____

Company Name: Coastal Fuels Marketing
Facility Name: Cape Canaveral
Street Address: 8954 N. Atlantic Ave
City: Cape Canaveral State: FL Zip: 32920

Process: Heater Unit #: 4 Operating Mode: High Fire
Control Equipment: NA Operating Mode: NA

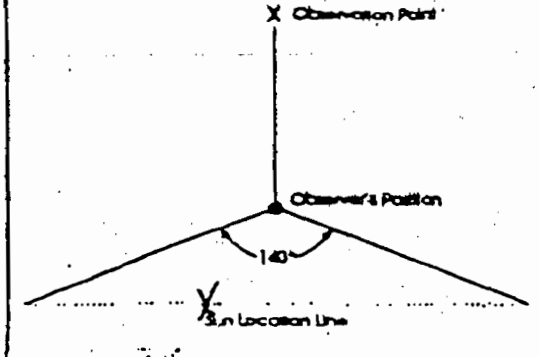
Describe Emission Point: stack w/ rain cap
Height of Emiss. Pt.: ~30ft Height of Emiss. Pt. Rel. to Observer: ~27ft
Distance to Emiss. Pt.: ~80ft Direction to Emiss. Pt. (Degrees): W 290°

Describe Emissions: None Observed
Emission Color: NA Water Droplet Plume: Attached ☐ Detached ☐ None ☒

Describe Plume Background: sky
Background Color: white/gray Sky Conditions: cloudy
Wind Speed: 5-10 mph Wind Direction: South
Ambient Temp.: ~ 70°F

Source Layout Sketch — Draw North Arrow

See page one for diagram
Observer location did not change



Additional Information:

Observation Date: 3/30/01 Start Time: 11:15AM End Time: 11:45 AM

Sec / Min	0	15	30	45	Comments
1	0	0	0	0	
2	0	0	0	0	
3	0	0	0	0	
4	0	0	0	0	
5	0	0	0	0	
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
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23	0	0	0	0	
24	0	0	0	0	
25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

Observer's Name (Print): Jim Estler
Observer Signature: [signature] Date: 3/30/01
Organization: Clean Air Consulting
Certified By: FDEP Date: Feb 2001

VISIBLE EMISSION OBSERVATION

Heater No. 5 Page 1 of 2

Method Used: Method 9 / Other: _____

Company Name: Coastal Fuels Marketing
Facility Name: Cape Canaveral
Street Address: 8954 N. Atlantic Blvd
City: Cape Canaveral | State: FL | Zip: 32920

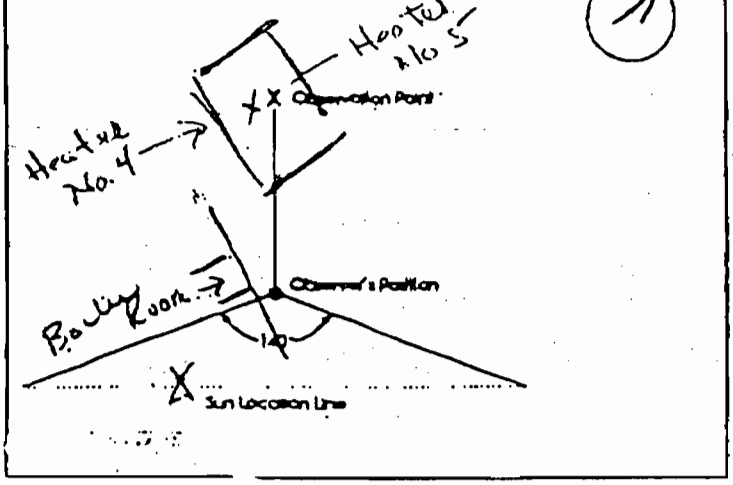
Process: Heater | Unit #: 5 | Operating Mode: High Fire
Control Equipment: NA | Operating Mode: NA

Describe Emission Point: Stack w/ rain cap
Height of Emiss. Pt.: ~30ft | Height of Emiss. Pt. Rel. to Observer: ~27ft
Distance to Emiss. Pt.: ~85' | Direction to Emiss. Pt. (Degrees): W 266°

Describe Emissions: None Observed
Emission Color: NA | Water Droplet Plume: Attached ☐ Detached ☐ None ☒

Describe Plume Background: Sky
Background Color: white/blue | Sky Condition: Partly cloudy
Wind Speed: 5-10mph | Wind Direction: South
Ambient Temp.: ~70°F

Source Layout Sketch — Draw North Arrow



Observation Date: 3/30/01 | Start Time: 11:50AM | End Time: 12:20 PM

Sec / Min	0	15	30	45	Comments
1	0	0	0	0	
2	0	0	0	0	
3	0	0	0	0	
4	0	0	0	0	
5	0	0	0	0	
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
12	0	0	0	0	
13	0	0	0	0	
14	0	0	0	0	
15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
18	0	0	0	0	
19	0	0	0	0	
20	0	0	0	0	
21	0	0	0	0	
22	0	0	0	0	
23	0	0	0	0	
24	0	0	0	0	
25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

Additional Information: Heater taken to high fire on No. 2 fuel Oil (~43 gal/hr)

Observer's Name (Print): Jim Estler
Observer's Signature: _____ | Date: 3/30/01
Organization: Clean Air Consulting, Inc.
Certified By: FDEP | Date: Feb 2001

********** LABORATORY WORKSHEET **********
COASTAL DIESEL RECERTIFICATION
****

LAB NUMBER: 00213
LAB DATE: 02/06/01
****

PRODUCT : LOW SULFUR DIESEL
[illegible]KED : STK#7 AFTER SEVERN
LOCATION : CAPE CANAVERAL, FL.

JOB NO: FE-8102
SAMPLING DATE: 02/05/01

TERMINAL : COASTAL FUELS PAGE 1 CUSTOMER SPECS:

[RE]	[TEST_ID / TEST DESCRIPTION]	[ASTM]	[BY]	[RESULTS]
	00125 GRAVITY, API AT 60 F	D-1298	AM	37.6
	00228 SPECIFIC GRAVITY, AT 60 DEG F	D-1298	AM	0.8368
	00118 FLASH PT., PENSKY MARTENS, DEG F	D-93	RPA	158
	00237 SULFUR, X-RAY, WT PCT	D-4294	AM	0.0444
	00515 VISCOSITY, KINEMATIC @ 100 DEG F	D-445	RPA	2.832
	00267 WATER & SEDIMENT (S&W), VOL PCT	D-2709	RPA	0.005
	00053 CETANE INDEX (CALC.)	D-976	AM	52.4
	00084 DISTILLATION, IBP, DEG F	D-86	AM	352
	00086 RCVD, 10 PCT, DEG F		AM	424
	00091 RCVD, 50 PCT, DEG F		AM	519
	00096 RCVD, 90 PCT, DEG F		AM	606
	00099 END POINT, DEG F		AM	667
	00100 RECOVERY, VOL PCT		AM	99.0
	00101 RESIDUE, VOL PCT		AM	1.0
	00102 LOSS, VOL PCT		AM	0.0

VISIBLE EMISSION OBSERVATION

Heater No. 5 Page 2 of 2

Method 9 Other: _____

Company Name: Coastal Fuels Marketing
Facility Name: Cape Canaveral
Street Address: 8954 N. Atlantic Ave
City: Cape Canaveral State: FL Zip: 32920

Process: Heater Unit #: 5 Operating Mode: High Fire
Control Equipment: N.A. Operating Mode: NA

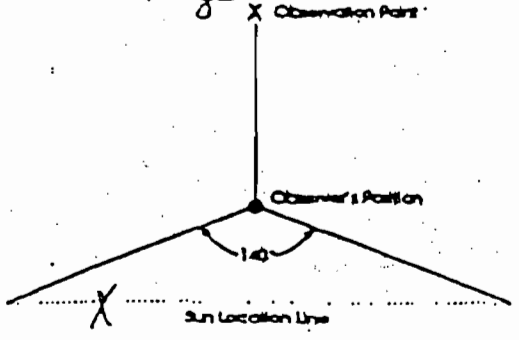
Describe Emission Point: stack w/ rain cap
Height of Emiss. Pt.: ~30 ft Height of Emiss. Pt. Rel. to Observer: ~27 ft
Distance to Emiss. Pt.: ~85 ft Direction to Emiss. Pt. (Degrees): W 298°

Describe Emissions: None Observed
Emission Color: NA Water Droplet Plume: Attached ☐ Detached ☐ None ☒

Describe Plume Background: sky
Background Color: Gray Sky Conditions: Overcast
Wind Speed: ~5-15 mph Wind Direction: South
Ambient Temp.: ~75° F ~73% H

Source Layout Sketch — Draw North Arrow

See page one for diagram Observer location did not change (1)



Additional Information:

Observation Date: 3/30/01 Start Time: 12:20 PM End Time: 12:50 PM

Sec Min	0	15	30	45	Comments
1	0	0	0	0	
2	0	0	0	0	
3	0	0	0	0	
4	0	0	0	0	
5	0	0	0	0	
6	0	0	0	0	
7	0	0	0	0	
8	0	0	0	0	
9	0	0	0	0	
10	0	0	0	0	
11	0	0	0	0	
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15	0	0	0	0	
16	0	0	0	0	
17	0	0	0	0	
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22	0	0	0	0	
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25	0	0	0	0	
26	0	0	0	0	
27	0	0	0	0	
28	0	0	0	0	
29	0	0	0	0	
30	0	0	0	0	

Observer's Name (Print): Jim Estler
Observer's Signature: [signature] Date: 3/30/01
Organization: Clean Air Consulting, Inc
Certified By: FDEP Date: Feb 2001