

# HISTORY OF PERMIT SUBMISSION

125,000 population Bay Co  
 2.6 million cu m fee to Wash  
 tipping fee of \$30/ton  
 to be paid when

- 0 MARCH 1984  
 ORIGINAL APPLICATION SUBMITTED
- 0 APRIL 1984  
 LETTER FROM DER TO BAY COUNTY  
 ASKING QUESTIONS
- 0 MAY 1984  
 RESPONSE TO QUESTIONS AND APPLICATION  
 RESUBMITTED
- 0 SEPTEMBER 1984  
 CONSTRUCTION PERMIT ISSUED

provisional

max SO<sub>2</sub> : 200  
 170

CEM  
 24 hr/d       $\frac{AV}{123}$

149 highest daily average      250-40 PPM for 1 hr.  
 80 PPM

100-150 ppm for SO<sub>2</sub>

HCl 800 highest  
 150 lowest  
 $\bar{x} = 467$  PPM

6 mos downtown  
 Newstack \$800,000  
 more precip \$500,000

plant cost \$38,000,000  
 been operating for 1 year

WEAST 5000 BTU/lb  
 PC waste 4450 BTU/lb

2000 ft by SO<sub>2</sub>  
 from powerplant 15 miles away  
 in rural area.

## PERMIT SUBMISSION PROGRAM

- 0 SUBMIT PSD PERMIT FOR ACTUAL WASTE  
COMMITTED 350 TPD MSW AND 178 TPD  
WOOD WASTE
  
- 0 PLANT DESIGNED TO BURN 510 TPD MSW
  
- 0 FACILITY DESIGNED TO HANDLE BAY COUNTY  
WASTE IN THE YEAR 2000
  
- 0 RESUBMIT PERMIT APPLICATION AFTER  
STARTUP TO OBTAIN 510 TPD PERMIT.

PERMIT APPLICATION TO BURN 510 TPD MSW

- o 1984 CONSTRUCTION PERMIT -  
350 TPD MAXIMUM
  
- o JUNE 1987 - VERIFY EMISSION ESTIMATES  
AND PREPARE APPLICATION TO OBTAIN  
520 TPD PERMIT
  
- o FALL 1987 - DISCUSSIONS WITH DER
  
- o JANUARY 1988 - PERMIT SUBMITTAL

**EMISSION ESTIMATES USED  
IN PERMIT APPLICATIONS**

- 0 ORIGINAL EMISSION ESTIMATES BASED ON LIMITED DATA**
  - GALLATIN, TN FACILITY**
  - KURE CITY, JAPAN**
  
- 0 BAY COUNTY EMISSION ESTIMATES TO BE VERIFIED AT START-UP**
  
- 0 PLUG ACTUAL MEASUREMENTS INTO DER CONSTRUCTION PERMIT APPLICATION -- PERMIT TO BURN AT DESIGN RATED CAPACITY OF 510 TPD**

ATTACHMENT D

BAY COUNTY RESOURCE MANAGEMENT CENTER REVISED EMISSION ESTIMATES

EMISSION ESTIMATES

Emission factors and estimated annual emission rates for various pollutants were prepared and submitted to the Florida DER in the facility's permit application in 1984. Table 1 contains the emission estimates for particulate matter, CO, NO<sub>x</sub>, SO<sub>2</sub>, HC and lead. These estimates were based on worst case air pollution conditions for each pollutant; i.e. for SO<sub>2</sub> 350 TPD MSW and 135 TPD woodchips; for NO<sub>x</sub>, CO, and HC, 250 TPD MSW and 220 TPD wood chips.

TABLE 1  
PERMITTED EMISSION RATES  
BURNING MSW AND WOOD WASTE

<u>Pollutant</u>	<u>Annual Emissions (tons/year per train)</u>	<u>Total Annual Emissions (tons/year - 2 trains)</u>
Particulate Matter	25	50
CO	505	1010
NO <sub>x</sub>	107	214
SO <sub>2</sub>	96	192
Pb	0.15	0.3
HC	39	78
Hg(1)	0.64	1.28

(1) - This was permitted for burning sewage sludge.  
Note: No sewage sludge will be incinerated.

Emission factors for burning 510 TPD of MSW with a heating value of 4500 Btu/lb are given in Table 2. These emission factors are based, in part, on the recent test results at Bay County, as well as previous emission test data and/or emission factors proposed at other waste-to-energy facilities.

TABLE 3  
ESTIMATED ANNUAL EMISSIONS USING 1987 DEVELOPED EMISSION FACTORS

<u>Pollutant</u>	<u>Emission Factor (Wood Chips)</u>	<u>Emission Factor (MSW)</u>	<u>Annual Emissions (tons/year) Based on 350 TPD MSW 135 TPD Wood</u>	<u>Annual Emissions (tons/year) Based on 510 TPD MSW</u>	<u>Difference (tons/year)</u>
Particulate Matter	0.03 gr/dscf	0.03 gr/dscf	50 <sup>1</sup>	59 <sup>2</sup>	9
CO	20 lb/ton	3.58 lb/ton	722	333	-389
NO <sub>x</sub>	2.8 lb/ton	2.41 lb/ton	223	224	1
SO <sub>2</sub>	0.3 lb/ton	3.36 lb/ton	223	313	90
HC	1.7 lb/ton	0.196 lb/ton	54	18	-36
Pb	0	0.0039 lb/ton	0.25	0.36	0.11
Hg	0	0.0017 lb/ton	0.11	0.16	0.05
Be	0	4.8x10 <sup>-7</sup> lb/ton	3.1x10 <sup>-5</sup>	4.5x10 <sup>-5</sup>	1.36x10 <sup>-5</sup>

1 - Based on a gas flow rate of 22,280 dscf/min per train (from the 1984 permit application).

2 - Based on a gas flow rate of 26,300 dscf/min per train (Bay County Test Data).

TABLE 4  
HCl Emission Factors For The Bay County W-T-E Plant Burning 510 TPD of MSW  
That has a Heating Value of 4500 Btu/lb (365 days per year)

Pollutant	Emission Test Results 4/87-6/87 per train corrected to 12% CO <sub>2</sub>	Typical Emission Factors Concentration Corrected to 12% CO <sub>2</sub>	lb/10 <sup>6</sup> Btu (500 ppm)	lb/ton (500 ppm)
HCl	467 ppm	500 ppm	0.64	5.8

TABLE 5  
Estimated Annual HCl Emissions Using 1987 Developed Emission Factor

Pollutant	Emission Factor (wood chips)	Emission Factor (MSW)	Annual Emissions (tons/year) Based on 350 TPD (MSW) 135 TPD Wood	Annual Emissions (tons/year) Based on 510 TPD MSW	Difference tons/year
HCl	0	5.8 lb/ton	370	540	170

ATTACHMENT E  
BEST AVAILABLE CONTROL TECHNOLOGY

The basic control technology requirement for new and modified major sources is the application and evaluation of BACT. BACT is defined as "an emission limitation based on the maximum degree of reduction for any regulated contaminant emitted from or which results from any regulated facility which the Department on a case-by-case basis, taking into account energy, environmental, and economic impacts and other costs, determines is achievable for such facility through an application of control of production processes and available methods, systems, and techniques for each such contaminant."

A major stationary source must apply BACT for all regulated pollutants emitted in significant quantities, as defined by de minimis emission rates (see Table 1).

TABLE 1  
ESTIMATED EMISSION RATES (WHEN INCREASING TO 510 TPD MSW FROM 350 TPD)  
COMPARED TO DE MINIMIS LEVELS

<u>Pollutant</u>	<u>Annual Increase TPY</u>	<u>De Minimis Rate TPY</u>
Particulate Matter	9	25
Carbon Monoxide	0	100
Nitrogen Oxide	0	40.0
Sulfur Dioxide	90	40.0
Hydrocarbons (Ozone)	0	40.0
Lead	0.11	0.6
Mercury	0.05	0.1
Beryllium	$1.36 \times 10^{-5}$	$4.0 \times 10^{-4}$



## BACT ACID GAS CONTROL COST ESTIMATES

	<u>SPRAY DRYER</u>	<i>20-40% reduction</i> <u>DRY INJECTION (FLUE GAS)</u>	<u>DRY INJECTION (COMBUSTOR)</u>
CAPITAL COST	\$2,338,000	\$1,275,000	\$875,000
OPERATING AND MAINTENANCE COSTS	\$283,773	\$510,980	\$510,980
LOST REVENUE EQUIVALENT	\$501,200	\$501,200	\$250,600
UNIFORM ANNUAL COST <i>10% for 20 yrs</i>	\$617,379	\$719,684	\$643,238

TABLE 6  
ADD-ON SPRAY DRYER CAPITAL COST ESTIMATE

Capital Cost:	\$1,863,000	-	Spray Dryers
	<u>\$ 475,000</u>	-	Drag Conveyors
TOTAL	\$2,338,000		

Cost Breakdown Includes:

- Engineering
- Foundations and Supports
- 2 Spray Dryers
- 3 Rotary Atomizers (1 spare for two trains)
- 2 Drag Conveyors
- Lime Storage Bins and Slaker
- Piping
- Ductwork
- Insulation
- Shipping to the Site
- Installation
- Start-up Services

TABLE 7  
ANNUAL OPERATING AND MAINTENANCE COST

	<u>Each Train</u>	<u>Cost</u>	<u>Cost per Year For Both Trains</u>
Lime	115 lb/hr	\$75/ton	\$ 75,555
Power for Spray Dryer	30 kw	\$0.05/kwh	\$ 26,280
Power for Delta P (fan cost)	Delta P=3.5 in H <sub>2</sub> O Gas Flow-55,000 acfm for each unit	(see below)	\$ 30,438

$$\text{Fan Power} = Q \times \frac{0.7456}{6356 \times E} \times \text{Delta P} \times H$$

where: P = fan power (kwh)  
 Q = gas volume (acfm)  
 E = fan efficiency (assumed 0.65)  
 Delta P = pressure drop  
 H = annual operating rate (8760 hr/yr)

Water Cost		\$ 5,440
Routine Maintenance 880 hr per spray dryer @ \$20/hr		\$ 35,200
SPARE PARTS Atomizer-bearings, inserts, packing, oil pump, seals washers, etc.		\$ 50,140
Lime slaking system		\$ 28,140
INCREASE DISPOSAL Costs 1629 tpy Residue @ \$20/ton		<u>\$ 32,580</u>
<b>TOTAL</b>		<b>\$283,773</b>

Table 8 shows the revenues that would be lost during a 4-week shutdown (for each combustor/boiler train) because of the retrofit of the spray dryer and the mechanical drag conveyors.

TABLE 8  
Lost Revenues Because of Plant Shutdown  
During Scrubber Installation

Assume: 4 weeks shutdown per train

Lost Electrical Revenue	\$ 403,200
By-Pass Waste Costs	<u>\$ 98,000</u>
(350 TPD x 28 days x \$10/ton)	
	\$ 501,200

Table 9 illustrates that the equivalent uniform annual cost (EUAC) for retrofitting acid gas controls is \$617,379.

TABLE 9  
Equivalent Uniform Annual Cost (EUAC) for  
Addition of Acid Gas Controls  
(i=10%, N=20 yrs)

Capital Cost	\$2,338,000	(Table 6)
Lost Revenue	<u>\$ 501,200</u>	(Table 8)
Total Cost	\$2,839,200	

**Operation & Maintenance - \$283,773 (Table 7)**

EUAC = \$2,839,200 (A/P, 10%, 20) + \$283,773

EUAC = \$ 617,379

TABLE 1  
ADD-ON DRY INJECTION SYSTEM CAPITAL COST ESTIMATE

Capital Cost:   \$ 800,000 - Spray Dryers  
                  \$ 475,000 - Drag Conveyors  
TOTAL:       \$1,275,000

Cost Breakdown Includes:   Engineering  
                                  Foundations and Supports  
                                  2 Rotary Screw Feeders  
                                  Mixing Vanes  
                                  2 Drag Conveyors  
                                  Lime Storage Silo  
                                  Shipping to the Site  
                                  Installation  
                                  Start-up Services

TABLE 2  
ANNUAL OPERATING AND MAINTENANCE COST

	<u>Each Train</u>	<u>Cost</u>	<u>Cost per Year For Both Trains</u>
Lime	500 lb/hr	\$75/ton	\$328,500
Power for Rotary Feeder	30 kw	\$0.05/kwh	\$ 26,280
Power for Delta P (fan cost)	Delta P=2.0 in H <sub>2</sub> O (see below) Gas Flow-55,000 acfm for each unit (@ 0.05/kwh)		\$ 17,400

$$\text{Fan Power} = Q \times \frac{0.7456}{6356 \times E} \times \text{Delta P} \times H$$

- where: P = fan power (kwh)  
 Q = gas volume (acfm)  
 E = fan efficiency (assumed 0.65)  
 Delta P = pressure drop  
 H = annual operating rate (8760 hr/yr)

Water Cost	\$ - 0 -
Routine Maintenance 220 hr per injection system @ \$20/hr	\$ 8,800
Spare Parts	\$ 10,000
Increase Disposal Costs 6000 tpy Residue @ \$20/ton	<u>\$120,000</u>
<b>TOTAL:</b>	<b>\$510,980</b>

TABLE 3  
 LOST REVENUES BECAUSE OF PLANT SHUTDOWN  
 DURING DRY INJECTION SYSTEM INSTALLATION

Assume: 4 weeks shutdown per train

Lost Electrical Revenue:	\$ 403,200
By-Pass Waste Costs:	\$ <u>98,000</u>
(350 TPD x 28 days x \$10/ton)	
	\$ 501,200

TABLE 4  
 EQUIVALENT UNIFORM ANNUAL COST (EUAC) FOR  
 ADDITION OF A DRY INJECTION SYSTEM  
 (i=10%, N=20 yrs)

Capital Cost:	\$1,275,000	(Table 1)
Lost Revenue:	\$ <u>501,200</u>	(Table 8)
Total Cost:	\$1,776,200	
Operation & Maintenance:	\$ 510,890	(Table 2)
EUAC = \$1,776,200 (A/P, 10%, 20) + \$510,980		
EUAC = \$ 719,684		

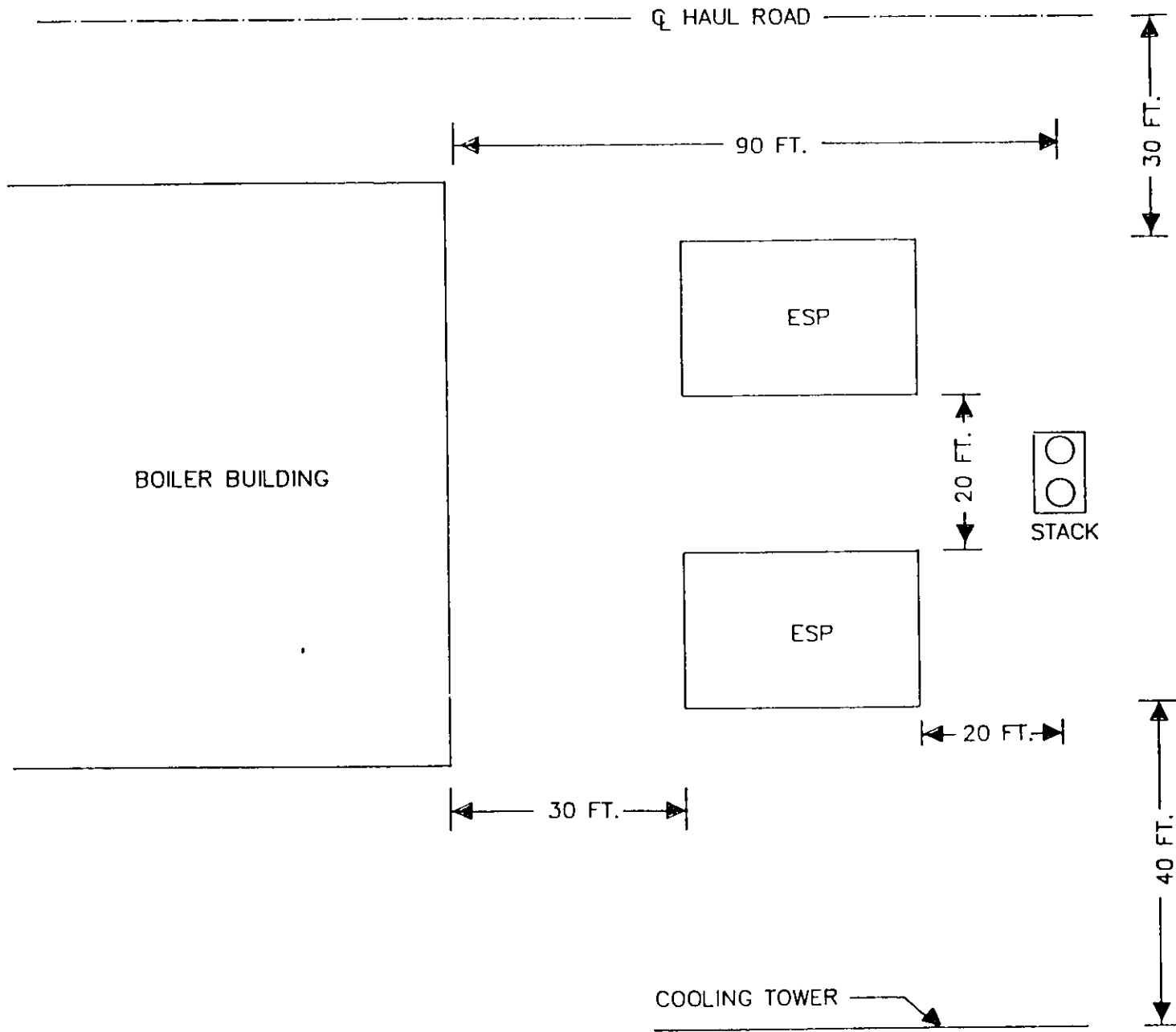
**BACT COSTS PER TON OF  
POLLUTANT REMOVED**

	<u>SPRAY DRYER</u>	<u>DRY INJECTION (FLUE GAS)</u>	<u>DRY INJECTION (COMBUSTOR)</u>
<b>SO<sub>2</sub> - \$/TON REMOVED (TONS REMOVED)</b>	<b>\$7000 90 TPY</b>	<b>\$12,000 - \$8000 60-90 TPY</b>	<b>\$11,000 - \$7200 60-90 TPY</b>
<b>HCL - \$/TON REMOVED (TONS REMOVED)</b>	<b>\$3700 170 TPY</b>	<b>\$4300 170 TPY</b>	<b>\$3800 170 TPY</b>

*2000 tons SO<sub>2</sub>*

*\$2400/ton*





## SUMMARY

- 0 BAY COUNTY FACILITY DESIGNED TO  
BURN 510 TPD
  
- 0 APPROXIMATELY 110 W-T-E FACILITIES  
IN U.S. THAT DO NOT HAVE ACID GAS  
SCRUBBERS
  
- 0 EPA OR STATE AGENCIES HAVE NOT REQUIRED  
ACID GAS SCRUBBERS TO BE RETROFITTED