Department of Environmental Protection

Jeb Bush
Governor

Northwest District
160 Governmental Center
Pensacola, Florida 32501-5794

David B. Struhs
Secretary

FAX TRANSMITTAL FORM

TO: Bruce Mitchell
DARM

FAX #: SC) 292 6979

DATE: 3/20/02 - HAPPY SPRING!

FROM: MB Cuda
FDEP Northwest District Air Program

PHONE: 850/595-8364, extension 1220
Fax 850/595-8096

Stone AC Permit, as requested

Number of pages including transmittal form: 9

Faxed by: MBC

Department of Environmental Protection

FILE COPY

Lawton Chiles
Governor

Northwest District
160 Governmental Center
Pensacola, Florida 32501-5794

Virginia B. Wetherell
Secretary

June 11, 1996

David Riley
Stone Container Corporation
1 Everitt Avenue
Panama City, Florida 32402

Dear Mr. Riley:

This is in response to Mr. David Buff's May 24 letter requesting that permits AO-03270940 and AC03-252285 be amended regarding the maximum allowable operating rate of 120 TPH ADUP in the previous permits. The 87.3 TPH used in specific condition 2 was taken from page 12 of your AO application as the maximum production rate, but since the production can not be tracked on an hourly basis due to the sequencing of the 22 digesters, an average rate should not be used as a maximum allowable.

This letter can be used as a clarifying amendment to the permits restoring the 120 TPH limit as requested and, for PSD purposes, the annual production rate of the digester system remains at 668,850 tons of air dry unbleached pulp (ADUP) per year.

If you have any comments or questions please contact Andy Allen at (904) 444-8364.

Sincerely,

Ed K. Middleswart

Ed K. Middleswart, P.E.
Air Program Administrator

EKM:aac

cc: DEP Division of Air Resources Management, Tallahassee

PCBO

Department of Environmental Protection

Lawton Chiles
Governor

Northwest District
160 Governmental Center
Pensacola, Florida 32501-5794

Virginia B. Wetherell
Secretary

PERMITTEE:

Stone Container Corporation

I.D. Number: 10PCY03000927
Permit/Certification Number: AC03-252285
Date of Issue: July 5, 1994
Expiration Date: June 15, 1995
County: Bay
Latitude/Longitude:30°08'30"N/85°37'25"W
Project: Digester System Rebuild

This permit is issued under the provisions of section 403.087,Florida Statutes, and Florida Administrative Code Rules 17-296, 17-297 and 17-4. The above named applicant, hereinafter called permittee, is hereby authorized to perform the work or operate the facility shown on the application and approved drawings, plans, and other documents attached hereto or on file with the Department and made a part hereof and specifically described as follows:

The 22 digester systems will be replaced in kind and the emissions will be totally contained in the existing NCG collection system and routed to the lime kiln for incineration. The No. 4 Bark Boiler serves as backup to the lime kiln for TRS incineration. The TRS gases will be subjected to a minimum temperature of 1200 degrees Fahrenheit for at least 0.5 seconds in either of the two combustion devices. The 22 batch digester systems consist of five blow tanks, one accumulator tank with a condenser before and after the accumulator tank and a turpentine condensing system following the accumulator. The maximum process rate will not increase as a result of the new digester system.

The project is located at the permittee's kraft pulp mill in Panama City, Bay County, Florida. The UTM coordinates are zone 16, 632.8 km East, and 3335.1 km North.

The Standard Industrial Codes are:
Industry No. 2611-Pulp Mills
~~Industry No. 2621-Paper Mills~~ L.M.,

The Standard Classification Codes are:
Pulp and Paper Industry Major Group 26:
Sulfate (Kraft) Pulping
BATCH DIGESTER SYSTEM 3-07-001-01
TERPENE CONDENSER 3-07-001-07

PERMITTEE:

Stone Container Corporation

I.D. Number: 10PCY03000927
Permit/Certification Number: AC03-252285
Date of Issue: July 5, 1994
Expiration Date: June 15, 1995

SPECIFIC CONDITIONS:

General

1. The attached General Conditions are part of this permit. [FAC Rule 17-4.160]

Construction

2. The Department shall be notified upon initial commissioning of the new Digester system. [FAC Rule 17-4.210]

3. The Department shall be notified and prior approval obtained of any changes or revisions from the June 6, 1994 application. [FAC Rule 17-4.210]

Operation

4. The digester system may operate continuously (8760 hours per year). [FAC Rule 17-4.070]

5. The maximum production rate will be 87.3 tons per hour air dried unbleached pulp (ADUP). [FAC Rule 17-4.070]

6. The non-condensible gases (NCG) from the batch digesters, blow tanks, accumulator tank and turpentine condenser system shall be destroyed in the Lime Kiln or the Bark Boiler by subjecting the TRS gases to at least 1200°F for at least 0.5 seconds. [FAC Rule 17-296.404(3)(e)]

7. The digester system is subject to the total reduced sulfur (TRS) emission limiting standard which requires combustion of the TRS gases in the lime kiln. [FAC Rule 17-296.404(3)(a)1]

Administrative

8. Submit an updated TRS VENTING CONTINGENCY PLAN with the request for the operation permit. The plan shall include definitions of what constitutes a reportable venting incident and an assessment of the use of the back-up control device.[17-296.404(3)3]

9. The new process equipment shall be installed in such a manner to facilitate regular inspections and maintenance to minimize fugitive gaseous emissions. [FAC Rule 17-4.070]

10. An annual operation report shall be submitted by March 1 each year. [FAC Rule 17-210.370]

11. A major air pollution source Annual Operation Fee Form must be completed and submitted with the appropriate fee between January 15 and March 1 of each year.[FAC Rule 17-213]

PERMITTEE:

Stone Container Corporation

I.D. Number: 10PCY03000927
Permit/Certification Number: AC03-252285
Date of Issue: July 5, 1994
Expiration Date: June 15, 1995

SPECIFIC CONDITIONS:

12. The applicant shall retain a Professional Engineer registered in the State of Florida, for the inspection of the construction of this project. Upon completion the engineer shall inspect for conformity to the permit application and associated documents. A certificate of completion shall be submitted with the compliance test results for an operation permit. The permittee shall obtain an operating permit for this source before the expiration of this construction permit if the permittee desires to continue operation.[FAC Rule 17-4.050]

13. The permanent source identification number for this point source is 10PCY03000927. Please cite this number on all test reports and other correspondence specific to this permitted point source.[FAC Rule 17-297.570]

14. The Department telephone number for reporting problems, malfunctions or exceedances under this permit is (904) 444-8300, day or night, and for emergencies involving a significant threat to human health or the environment is (904) 488-1320. For routine business, telephone (904) 872-4375 during normal working hours. [FAC Rule 17-210.700]

Expiration Date:

June 15, 1995

Issued this 5th day of July, 1994.

STATE OF FLORIDA DEPARTMENT
OF ENVIRONMENTAL PROTECTION

Ed K. Middleton
for BOBBY A. COOLEY
District Director

PERMITTEE:

Stone Container Corporation

I.D. Number: 10PCY03000927
Permit/Certification Number: AC03-252285
Expiration Date: June 15, 1995

GENERAL CONDITIONS:

1. The terms, conditions, requirements, limitations, and restrictions set forth in this permit are "permit conditions", and are binding and enforceable pursuant to Sections 403.141, 403.727, or 403.859 through 403.861, Florida Statutes. The permittee is placed on notice that the Department will review this permit periodically and may initiate enforcement action for any violation of these conditions.

2. This permit is valid only for the specific processes and operations applied for and indicated in the approved drawings or exhibits. Any unauthorized deviation from the approved drawings, exhibits, specifications, or conditions of this permit may constitute grounds for revocation and enforcement action by the Department.

3. As provided in Subsections 403.087(6) and 403.722(5), Florida Statutes, the issuance of this permit does not convey any vested rights or any exclusive privileges. Nor does it authorize any injury to public or private property or any invasion of personal rights, nor any infringement of federal, state or local laws or regulations. This permit does not constitute a waiver of or approval of any other Department permit that may be required for other aspects of the total project which are not addressed in the permit.

4. This permit conveys no title to land or water, does not constitute state recognition or acknowledgment of title, and does not constitute authority for the use of submerged lands unless herein provided and the necessary title or leasehold interests have been obtained from the state. Only the Trustees of the Internal Improvement Trust Fund may express state opinion as to title.

5. This permit does not relieve the permittee from liability for harm or injury to human health or welfare, animal, or plant life, or property caused by the construction or operation of this permitted source, or from penalties therefore; nor does it allow the permittee to cause pollution in contravention of Florida Statutes and Department rules, unless specifically authorized by an order from the Department.

6. The permittee shall properly operate and maintain the facility and systems of treatment and control (and related appurtenances) that are installed and used by the permittee to achieve compliance with the conditions of this permit, are required by Department rules. This provision includes the operation of backup or auxiliary facilities or similar systems when necessary to achieve compliance with the conditions of the permit and when required by Department rules.

7. The permittee, by accepting this permit, specifically agrees to allow authorized Department personnel, upon presentation of credentials or other documents as may be required by law and at a reasonable time, access to the premises where the permitted activity is located or conducted to:

a. Have access to and copy any records that must be kept under the conditions of this permit;

b. Inspect the facility, equipment, practices, or operations regulated or required under this permit; and,

PERMITTEE:

Stone Container Corporation

I.D. Number: 10PCY03000927
Permit/Certification Number: AC03-252285
Expiration Date: June 15, 1995

GENERAL CONDITIONS:

c. Sample or monitor any substances or parameters at any location reasonably necessary to assure compliance with this permit or Department rules.

Reasonable time may depend on the nature of the concern being investigated.

8. If, for any reason, the permittee does not comply with or will be unable to comply with any condition or limitation specified in this permit, the permittee shall immediately provide the Department with the following information:

a. A description of and cause of noncompliance; and

b. The period of noncompliance, including exact dates and times; or, if not corrected, the anticipated time the noncompliance is expected to continue, and steps being taken to reduce, eliminate, and prevent recurrence of the noncompliance.

The permittee shall be responsible for any and all damages which may result and may be subject to enforcement action by the Department for penalties or for revocation of this permit.

9. In accepting this permit, the permittee understands and agrees that all records, notes, monitoring data and other information relating to the construction or operation of this permitted source which are submitted to the Department may be used by the Department as evidence in any enforcement case involving the permitted source arising under the Florida Statutes or Department rules, except where such use is proscribed by Sections 403.73 and 403.111, Florida Statutes. Such evidence shall only be used to the extent it is consistent with Florida Rules of Civil Procedure and appropriate evidentiary rules.

10. The permittee agrees to comply with changes in Department rules and Florida Statutes after a reasonable time for compliance, provided however, the permittee does not waive any other rights granted by Florida Statutes or Department rules.

11. This permit is transferable only upon Department approval in accordance with Florida Administrative Code Rules 17-4.120 and 17-730.300, as applicable. The permittee shall be liable for any noncompliance of the permitted activity until the transfer is approved by the Department.

12. This permit or a copy thereof is required to be kept at the work site of the permitted activity.

13. The permittee shall comply with the following:

a. Upon request, the permittee shall furnish all records and plans required under Department rules. During enforcement actions, the retention period for all records will be extended automatically unless otherwise stipulated by the Department.

PERMITTEE:

Stone Container Corporation

I.D. Number: 10PCY03000927
Permit/Certification Number: AC03-252285
Expiration Date: June 15, 1995

GENERAL CONDITIONS:

b. The permittee shall hold at the facility or other location designated by this permit records of all monitoring information (including all calibration and maintenance records and all original strip chart recordings for continuousmonitoring instrumentation) required by the permit, copies of all reports required by this permit, and records of all data used to complete the application for this permit. These materials shall be retained at least three years from the date of the sample, measurement, report or application unless otherwise specified by Department rule.

c. Records of monitoring information shall include:

- the date, exact place, and time of sampling or measurement;
- the person responsible for performing the sampling or measurement;
- the date(s) analyses were performed;
- the person responsible for performing the analyses;
- the analytical techniques or methods used; and
- the results of such analyses.

14. When requested by the Department, the permittee shall within a reasonable time furnish any information required by law which is needed to determine compliance with the permit. If the permittee becomes aware the relevant facts were not submitted or were incorrect in the permit application or in any report to the Department, such facts or information shall be corrected promptly.

Memorandum

Florida Department of Environmental Protection

TO: Bobby A. Cooley
THROUGH: Ed K. Middleswart, P.E.
FROM: Andy Allen
DATE : June 13, 1994
SUBJECT: Evaluation Summary for Stone Container Corporation
Construction Permit to rebuild the Digester System

I recommend issuing a construction permit to reconstruct the 22 digester systems as a result of the April 13 catastrophic failure of one of the batch digesters. The public notice for the project was published June 20. Construction has begun because Stone assumed no construction permit would be required since they were replacing equipment damaged by the explosion. The TRS gases from the digester system are combusted in a lime kiln which is not subject to 40 CFR 60.283, therefore the construction permit has no impact on emission limits.

Process Description

The 22 digester systems will be replaced in kind and the emissions will be totally contained in the existing NCG collection system and routed to the lime kiln for incineration. The No. 4 Bark Boiler serves as backup to the lime kiln for TRS incineration. The TRS gases will be subjected to a minimum temperature of 1200 degrees Fahrenheit for at least 0.5 seconds in either of the two combustion devices. The 22 batch digester systems consist of five blow tanks, one accumulator tank with a condenser before and after the accumulator tank and a turpentine condensing system following the accumulator. The maximum processing rate will not increase as a result of the new digester systems.

Pollution Control Equipment

The emissions are incinerated in the lime kiln and the No. 4 Bark Boiler is backup.

Applicable Rules & Regulations and Environmental Impact

This source is regulated under provisions of Section 403.087, Florida Statutes and Florida Administrative Code Rules 17-296, 17-297, and 17-4. The system is presently permitted to operate under A003-174790 and the rebuild does not increase emissions since the emissions are incinerated in the existing lime kiln.

The exhaust gases from the lime kiln shall not contain TRS in excess of 20 ppmvd at standard conditions corrected to 10% oxygen as a 12-hour average.

Compliance Monitoring

The lime kiln has a TRS continuous emissions monitor.

Compliance History

Acceptable

ASA:aac

MEMORANDUM

TO : Ed K. Middleswart, P.E.
FROM : Andy Allen, Armando I. Sarasua
DATE : November 4, 1997
SUBJECT : Evaluation Summary for Stone Container Corporation, Woodyard Process Rate Increase 0050009030, Bay County

We recommend issuing notice of intent to issue a construction permit to Stone Container Corporation for a Woodyard Process Rate Increase from 355,118 cords roundwood and 416,812 cords chips to 710,160 and 609,840 cords per year respectively, plus 316,098 T/yr purchased bark. The woodyard is a portion of the SCC kraft paper mill. The mill is a major source and subject to Title V under the Clean Air Act.

Process Description Wood chips are used as the raw material in the papermaking process and scrap wood and bark are used in steam generation. Roundwood (whole tree trunks) is received as either shortwood or longwood. Purchased hardwood or softwood chips are also received. Bark is a byproduct of log processing and some bark is also purchased. The chipping process begins by passing logs through a debarker to remove bark, which is collected and transferred via conveyors and hogged to obtain a desired size. After processing the bark, it is stored in piles, transferred to the bark bin, and then used as a fuel for the boilers at the facility. The logs are then chipped and the chips screened for proper size. Both purchased and manufactured chips are conveyed and stored in chip reclaimer storage piles. The facility has one softwood chip reclaimer and one hardwood reclaimer storage pile where chips are stored temporarily until needed by the facility.

Pollution Control Equipment A single cyclone is associated with the bark transfer and conveying system, and used to pneumatically convey the bark. Conveyors are covered and roads are paved and maintained to minimize particulate entrainment. Four (4) cyclones are used in the Screening Room to separate pneumatically conveyed chips and fines from the conveying air stream.

Applicable Rules and Regulations and Environmental Impact A fee of $2,000 was submitted. The appropriate fee for an incremental increase of 4.8 T/yr, subtype 1F source, is $250 and permittee was advised to apply for a refund. This source is regulated in accordance with FAC Rule 62-296.320(4)(c) Fugitive Emissions and the General Visible Emissions limit of 20% under FAC Rule 62-296.320(4)(b) The potential to emit will increase 4.8 T/yr for particulate matter (PM) and 1.9 T/yr for PM10 (PM < 10 um), from 39.8 and 14.5 T/yr to 44.6 and 16.4 T/yr respectively.

Compliance Monitoring: None required by original AC01-148859.

Compliance History No problems noted in file.

EKM:asc

Florida Department of

Memorandum **Environmental Protection**

TO: Ed Middleswart

FROM: MB Curle

DATE: January 5, 1998

SUBJECT: Permit for Signature:
Stone Container (0050009-003-AC)

Intent to Issue with Public Notice issued on: November 6, 1997

Public Notice published on: December 19, 1997

Proof of publication received by the Dept. on: December 31, 1997

No petitions for hearing filed with OGC as of: January 5, 1998

(15 days up January 2, 1998)

STATE OF FLORIDA
DEPARTMENT OF ENVIRONMENTAL PROTECTION
NOTICE OF PERMIT

In the matter of an
Application for Permit
By:
Jack B. Prescott
General Manager
Stone Container Corporation
Post Office Box 2560
Panama City FL 32402

DEP File No. 0050009-003-AC
Bay County

Enclosed is Permit Number 0050009-003-AC, issued pursuant to Section 403.087, Florida Statutes.

Any party to this Order (permit) has the right to seek judicial review of the permit pursuant to Section 120.68, Florida Statutes, by the filing of a Notice of Appeal pursuant to Rule 9.110, Florida Rules of Appellate Procedure, with the Clerk of the Department in the Office of General Counsel, 3900 Commonwealth Boulevard, Tallahassee, Florida 32399-3000, and by filing a copy of the Notice of Appeal accompanied by the applicable filing fees with the appropriate District Court of Appeal. The Notice of Appeal must be filed within 30 days from the date this Notice is filed with the Clerk of the Department.

Executed in Pensacola, Florida.

State of Florida Department
of Environmental Protection

Ed K. Middleswart

ED K. MIDDLESWART, P.E.
Program Administrator

160 Governmental Center
Pensacola, Florida 32501-5794
(850) 595-8364

CERTIFICATE OF SERVICE

The undersigned duly designated deputy agency clerk hereby certifies that this NOTICE OF PERMIT and all copies were mailed before the close of business on January 5, 1998 to the listed persons.

FILING AND ACKNOWLEDGMENT FILED, on this date, pursuant to §120.52(11), Florida Statutes, with the designated Department clerk, receipt of which is hereby acknowledged.

Clerk [signature] Date 1/5/98

Copies Furnished to:
David A. Buff, P.E., Golder Associates, Inc.
DEP Division of Air Resources Management, Tallahassee
DEP Northwest District Branch Office, Panama City

Department of Environmental Protection

Lawton Chiles
Governor

Northwest District
160 Governmental Center
Pensacola, Florida 32501-5794

Virginia B. Wetherell
Secretary

PERMITTEE:

Stone Container Corporation

AIRS I.D. Number: 0050009
Air Permit Number: 0050009-003-AC
Emission Unit: 030
Date of Issue: JAN 05 1998
Expiration Date: March 1, 1998
County: Bay
Project: Woodyard Process Rate Increase

This permit is issued under the provisions of Section 403.087, Florida Statutes, and Florida Administrative Code Rules 62-296, 62-297 and 62-4. The above named applicant, hereinafter called Permittee, is hereby authorized to perform the work or operate the facility shown on the application and approved drawing(s), plans, and other documents attached hereto or on file with the Department and made a part hereof and specifically described as follows:

Construction permit to allow for increased emissions of a Woodyard Process Rate Increase: project is to simply increase the throughput of hardwood and softwood through the woodyard to allow increased productivity in the paper mill. No actual construction to take place.

Wood chips are used as the raw material in the papermaking process and scrap wood and bark are used in steam generation. The wood is processed in the woodyard prior to use in the mill. Roundwood (whole tree trunks) is received as either shortwood or longwood. Purchased hardwood or softwood chips are also received. Bark is a byproduct of log processing and some bark is also purchased.

Long wood and short wood is received and stored temporarily until processed. The chipping process begins by passing the logs through a debarker to remove the bark. The bark is collected and transferred via conveyors and hogged to obtain the desired size. Purchased bark is also delivered to the facility and processed. After processing the bark, it is stored in storage piles, transferred to the bark bin, and then to the boilers. This bark is used as a fuel for the boilers at the facility. A single cyclone is associated with the bark transfer and conveying system, and used to pneumatically convey the bark.

PERMITTEE:

Stone Container Corporation

AIRS I.D. Number: 0050009
Air Permit Number: 0050009-003-AC
Emission Unit: 030
Date of Issue: JAN 05 1998
Expiration Date: March 1, 1998

After the logs have passed through the debarker and the bark has been removed, they are sent to a chipper where they are chopped into the desired chip size. Chips are also received via truck or railcar and unloaded into a hopper. Both the purchased and manufactured chips are conveyed and stored in chip reclaimer storage piles. The facility has one softwood chip reclaimer and one hardwood reclaimer storage pile. The chips are stored in these piles temporarily until needed by the facility.

Prior to being sent to the mill, chips are reclaimed from the chip reclaimers and sent to the screen room building. Here, they are passed through screens to separate the various chip sizes. The oversized chips are passed through a slicer rechipper and recycled back through the screening system until the desired size is obtained. Four (4) cyclones are used in this area to separate pneumatically conveyed chips and fines from the conveying air stream. The chips are then transferred via conveyors and stored temporarily in the chip silos located in the pulping area until being sent to the mill by conveyor.

Construction shall be consistent with the construction permit application signed October 8, 1997.

Located: One Everitt Avenue, Panama City

PERMITTEE:

Stone Container Corporation

AIRS I.D. Number: 0050009
Air Permit Number: 0050009-003-AC
Emission Unit: 030
Date of Issue: JAN 05 1998
Expiration Date: March 1, 1998

SPECIFIC CONDITIONS:

General

1. The attached General Conditions are part of this permit. [FAC Rule 62-4.160]

Construction

2. The Department shall be notified upon commencement of construction (if any actual), and within 15 days of completion of construction. Annual status reports shall be provided no later than January 31 of each year reviewing the status of construction during the preceding year up to completion of the project. [FAC Rule 62-4.070]

3. The Department shall be notified and prior approval shall be obtained of any changes or revisions made during construction. [FAC Rule 62-4.030]

4. Satisfactory ladders, platforms and other safety devices as well as necessary parts shall be provided/made available to facilitate an adequate inspection program. [FAC Rule 62-297.310(6)]

Operation

5. The woodyard may operate continuously, i.e., 8760 hrs/yr, based on 24 hours/day, 7 days/week and 52 weeks per year. [FAC Rule 62-4.070 and construction permit application]

6. The maximum allowable operating rate, roundwood and purchased chips processed are:

roundwood	645,600 cords/year
purchased chips	554,400 cords/year

[FAC Rule 62-4.070 and construction permit application]

SPECIFIC CONDITIONS:

7. Reasonable precautions shall be taken to prevent emissions of unconfined particulate matter. Reasonable precautions shall include, but are not limited to, the following:

a. Maintenance of roads, parking areas and yards.
b. Application of water or other dust suppressants when necessary to control emissions.
c. Removal of particulate matter from roads and other paved areas under control of the owner or operator, and from buildings or work areas to prevent reentrainment.
d. Permittee will protect dust transfer points and transport and storage containers from wind action which might make dust airborne.
e. Chips manufactured on-site shall be screened following storage.
f. Chips will be screened following removal from storage prior to conveying to digesters.
g. All conveyor systems shall be covered or enclosed.
h. Drop distance from chip storage stacker shall be maintained to a minimum
i. All access roads shall be paved.

[FAC Rule 62-4.070, FAC Rule 62-296.320(4)(c)and Operating Permit AO03-190807]

Emissions

8. Visible emissions resulting from activities at the woodyard shall not be equal to, or greater than, 20% opacity. [FAC Rule 62-296.320(4)(b), DEP letter of December 4, 1995]

9. No objectionable odors shall be allowed off plant property. [FAC Rule 62-296.320(2)]

Testing

10. The Department can require special compliance tests in accordance with F.A.C. Rule 62-297.310(7)(b).

Administrative

11. An annual operating report for air pollutant emitting facility, DEP Form 62-210.990(5), shall be submitted by March 1 of each year. A copy of the form and instructions may be obtained from the Department of Environmental Protection, Northwest District Air Resources Management Program, (904) 444-8364. [FAC Rule 62-210.370(3)]

PERMITTEE:

Stone Container Corporation

AIRS I.D. Number: 0050009
Air Permit Number: 0050009-003-AC
Emission Unit: 030
Date of Issue: JAN 05 1998
Expiration Date: March 1, 1998

SPECIFIC CONDITIONS:

12. The applicant shall retain a Professional Engineer, registered in the State of Florida, for the inspection of this project. Upon project completion the engineer shall inspect for conformity to the permit application and associated documents. An updated Title V application (or pertinent updated sections) is to be submitted within 75 days of completion of the project but not later than January 1, 1998. The permittee shall obtain an initial or revised operating permit for this source before the expiration of this construction permit if the permittee desires to continue operation. [FAC Rule 62-210(300)]

13. In accordance with F.A.C. Rule 62-213, a Major Air Pollution Source Annual Operation Fee Form [DEP Form 62-213.900(1) attached] must be completed and submitted with appropriate fee between January 15 and March 1 of each year. If the Department has not received the fee payment by March 1, the Department shall impose, in addition to the fee, a penalty of 50 percent of the amount of the fee, plus interest on such amount computed in accordance with s.220.807, Florida Statutes. The Department may revoke any major air pollution source operation permit if it finds that the permit holder has failed to pay timely and required annual operation license fee, penalty or interest. The completed form and appropriate fees must be submitted to the Department of Environmental Protection, Title V Annual Emissions Fee, Cashiers Office, P.O. Box 3070, Tallahassee, Florida 32351-3070.

14. The emission unit covered by this permit, the woodyard facility, is assigned emissions unit number 0050009030. Please cite this number on all test reports and other correspondence specific to this permitted emission unit. [FAC Rule 62-297.310(8)]

15. The Department telephone number for reporting problems, malfunctions or exceedances under this permit is (850) 595-8364, day or night, and for emergencies involving a significant threat to human health or the environment is (800) 320-0519. For routine business, telephone (850) 872-4375 during normal working hours. [FAC Rule 62-4.130]

Expiration Date:

March 1, 1998

Issued this 5th day of JAN, 1998.

STATE OF FLORIDA DEPARTMENT
OF ENVIRONMENTAL PROTECTION

Ed K. Middleswart

ED K. MIDDLESWART, P.E.
Air Program Administrator

GENERAL CONDITIONS:

1. The terms, conditions, requirements, limitations, and restrictions set forth in this permit are "permit conditions", and are binding and enforceable pursuant to Sections 403.141, 403.727, or 403.859 through 403.861, Florida Statutes. The permittee is placed on notice that the Department will review this permit periodically and may initiate enforcement action for any violation of these conditions.

2. This permit is valid only for the specific processes and operations applied for and indicated in the approved drawings or exhibits. Any unauthorized deviation from the approved drawings, exhibits, specifications, or conditions of this permit may constitute grounds for revocation and enforcement action by the Department.

3. As provided in Subsections 403.087(6) and 403.722(5), Florida Statutes, the issuance of this permit does not convey any vested rights or any exclusive privileges. Nor does it authorize any injury to public or private property or any invasion of personal rights, nor any infringement of federal, state or local laws or regulations. This permit does not constitute a waiver of or approval of any other Department permit that may be required for other aspects of the total project which are not addressed in the permit.

4. This permit conveys no title to land or water, does not constitute state recognition or acknowledgment of title, and does not constitute authority for the use of submerged lands unless herein provided and the necessary title or leasehold interests have been obtained from the state. Only the Trustees of the Internal Improvement Trust Fund may express state opinion as to title.

5. This permit does not relieve the permittee from liability for harm or injury to human health or welfare, animal, or plant life, or property caused by the construction or operation of this permitted source, or from penalties therefore; nor does it allow the permittee to cause pollution in contravention of Florida Statutes and Department rules, unless specifically authorized by an order from the Department.

6. The permittee shall properly operate and maintain the facility and systems of treatment and control (and related appurtenances) that are installed and used by the permittee to achieve compliance with the conditions of this permit, are required by Department rules. This provision includes the operation of backup or auxiliary facilities or similar systems when necessary to achieve compliance with the conditions of the permit and when required by Department rules.

GENERAL CONDITIONS:

7. The permittee, by accepting this permit, specifically agrees to allow authorized Department personnel, upon presentation of credentials or other documents as may be required by law, access to the premises, at reasonable times, where the permitted activity is located or conducted for the purpose of:

a. Having access to and copying any records that must be kept under the conditions of this permit;
b. Inspecting the facility, equipment, practices, or operations regulated or required under this permit; and,
c. Sampling or monitoring any substances or parameters at any location reasonably necessary to assure compliance with this permit or Department rules.

Reasonable time may depend on the nature of the concern being investigated.

8. If, for any reason, the permittee does not comply with or will be unable to comply with any condition or limitation specified in this permit, the permittee shall immediately provide the Department with the following information:

a. A description of and cause of noncompliance; and
b. The period of noncompliance, including exact dates and times; or, if not corrected, the anticipated time the noncompliance is expected to continue, and steps being taken to reduce, eliminate, and prevent recurrence of the noncompliance. The permittee shall be responsible for any and all damages which may result and may be subject to enforcement action by the Department for penalties or for revocation of this permit.

9. In accepting this permit, the permittee understands and agrees that all records, notes, monitoring data and other information relating to the construction or operation of this permitted source which are submitted to the Department may be used by the Department as evidence in any enforcement case involving the permitted source arising under the Florida Statutes or Department rules, except where such use is proscribed by Sections 403.73 and 403.111, Florida Statutes. Such evidence shall only be used to the extent it is consistent with Florida Rules of Civil Procedure and appropriate evidentiary rules.

10. The permittee agrees to comply with changes in Department rules and Florida Statutes after a reasonable time for compliance, provided however, the permittee does not waive any other rights granted by Florida Statutes or Department rules.

GENERAL CONDITIONS:

11. This permit is transferable only upon Department approval in accordance with Florida Administrative Code Rules 62-4.120 and 62-730.300, as applicable.: The permittee shall be liable for any noncompliance of the permitted activity until the transfer is approved
by the Department.

12. This permit is required to be kept at the work site of the permitted activity during the entire period of construction or operation.

13. The permittee shall comply with the following:

a. Upon request, the permittee shall furnish all records and plans required under Department rules. During enforcement actions, the retention period for all records will be extended automatically unless otherwise stipulated by the Department.

b. The permittee shall hold at the facility or other location designated by this permit records of all monitoring information (including all calibration and maintenance records and all original strip chart recordings for continuous monitoring instrumentation) required by the permit, copies of all reports required by this permit, and records of all data used to complete the application for this permit. These materials shall be retained at least three years from the date of the sample, measurement, report or application unless otherwise specified by Department rule.

c. Records of monitoring information shall include:

- the date, exact place, and time of sampling or measurement;
- the person responsible for performing the sampling or measurement;
- the date(s) analyses were performed;
- the person responsible for performing the analyses;
- the analytical techniques or methods used; and
- the results of such analyses.

14. When requested by the Department, the permittee shall within a reasonable time furnish any information required by law which is needed to determine compliance with the permit. If the permittee becomes aware the relevant facts were not submitted or were incorrect in the permit application or in any report to the Department, such facts or information shall be corrected promptly.

?C Mill

5-21-02
Spokane Greg
Landing DAND

(1) lime kiln 85,000#/hr
69,486#/hr tested@ ⇒ 76,435 new op. limit

Oct 2001

(2) #1RB 123,700 #/hr tested@ 114,210

(3) #2RB 123,700 #/hr tested@ 114,090

(4) #1SDT 114,000

(5) #2SDT 115,210

Test Report

Oct 2000

(1) lime kiln 78,065 within 90%

(2) #1RB 117,750

(3) #2RB 117,570

(4) 112,440

(5) 113,100

Test Report

~~O: Comp. Enforcement~~

O: Comp. Enforcement
- Testing
- Companies
- Smith Sloan

FACILITY ID	NAME	EU ID	EU DESCRIPTION	YEAR	SCC
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1996	30700104
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1997	30700104
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1998	10200401
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1998	10200603
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1998	30700104
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1999	10200401
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1999	10200603
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1999	30700104
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	2000	10200401
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	2000	10200603
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	2000	30700104
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODUCE C	1996	30700106
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODUCE C	1997	30700106
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODUCE C	1998	30700106
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODUCE C	1998	39000403
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODUCE C	1998	39000603
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODUCE C	1999	30700106
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODUCE C	1999	39000403
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODUCE C	1999	39000603
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODUCE C	2000	30700106
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODUCE C	2000	39000403
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODUCE C	2000	39000603
0050009	PANAMA CITY MILL	5	LIME SLAKER	1996	30700199
0050009	PANAMA CITY MILL	5	LIME SLAKER	1997	30700199
0050009	PANAMA CITY MILL	5	LIME SLAKER	1998	30700199
0050009	PANAMA CITY MILL	5	LIME SLAKER	1999	30700199
0050009	PANAMA CITY MILL	5	LIME SLAKER	2000	30700199
0050009	PANAMA CITY MILL	14	POWER BOILER #5 (NONE)	1996	
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1996	10200401
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1996	10200603
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1996	10200901
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1997	10200401
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1997	10200603
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1997	10200901
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1998	10200401
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1998	10200603
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1998	10200901
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1999	10200401
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1999	10200603
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1999	10200901
0050009	PANAMA CITY MILL	15	BARK BOILER #3	2000	10200401
0050009	PANAMA CITY MILL	15	BARK BOILER #3	2000	10200602
0050009	PANAMA CITY MILL	15	BARK BOILER #3	2000	10200603
0050009	PANAMA CITY MILL	15	BARK BOILER #3	2000	10200901
0050009	PANAMA CITY MILL	16	BARK BOILER #4 (FLY ASH ARRESTOR & WE	1996	10200212
0050009	PANAMA CITY MILL	16	BARK BOILER #4 (FLY ASH ARRESTOR & WE	1996	10200401
0050009	PANAMA CITY MILL	16	BARK BOILER #4 (FLY ASH ARRESTOR & WE	1996	10200603
0050009	PANAMA CITY MILL	16	BARK BOILER #4 (FLY ASH ARRESTOR & WE	1996	10200901

0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	1997	10200212
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	1997	10200401
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	1997	10200603
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	1997	10200901
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	1998	10200212
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	1998	10200401
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	1998	10200603
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	1998	10200901
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	1999	10200212
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	1999	10200401
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	1999	10200603
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	1999	10200901
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	2000	10200212
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	2000	10200401
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	2000	10200603
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR & WE	2000	10200901
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FROM	1996	30700104
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FROM	1997	30700104
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FROM	1998	10200401
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FROM	1998	10200603
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FROM	1998	30700104
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FROM	1999	10200401
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FROM	1999	10200603
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FROM	1999	30700104
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FROM	2000	10200401
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FROM	2000	10200603
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FROM	2000	30700104
0050009	PANAMA CITY MILL	20 DISSOLVING TANK #2 (DEMISTER PADS)	1996	30700105
0050009	PANAMA CITY MILL	20 DISSOLVING TANK #2 (DEMISTER PADS)	1997	30700105
0050009	PANAMA CITY MILL	20 DISSOLVING TANK #2 (DEMISTER PADS)	1998	30700105
0050009	PANAMA CITY MILL	20 DISSOLVING TANK #2 (DEMISTER PADS)	1999	30700105
0050009	PANAMA CITY MILL	20 DISSOLVING TANK #2 (DEMISTER PADS)	2000	30700105
0050009	PANAMA CITY MILL	21 #1 SMELT DISSOLVING TANK (DEMISTER PA	1996	30700105
0050009	PANAMA CITY MILL	21 #1 SMELT DISSOLVING TANK (DEMISTER PA	1997	30700105
0050009	PANAMA CITY MILL	21 #1 SMELT DISSOLVING TANK (DEMISTER PA	1998	30700105
0050009	PANAMA CITY MILL	21 #1 SMELT DISSOLVING TANK (DEMISTER PA	1999	30700105
0050009	PANAMA CITY MILL	21 #1 SMELT DISSOLVING TANK (DEMISTER PA	2000	30700105
0050009	PANAMA CITY MILL	26 MULTIPLE EFFECT EVAPORATOR (MEE) SYS	1996	30700103
0050009	PANAMA CITY MILL	26 MULTIPLE EFFECT EVAPORATOR (MEE) SYS	1997	30700103
0050009	PANAMA CITY MILL	26 MULTIPLE EFFECT EVAPORATOR (MEE) SYS	1998	30700103
0050009	PANAMA CITY MILL	26 MULTIPLE EFFECT EVAPORATOR (MEE) SYS	1999	30700103
0050009	PANAMA CITY MILL	26 MULTIPLE EFFECT EVAPORATOR (MEE) SYS	2000	30700103
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOOD CH	1996	30700101
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOOD CH	1997	30700107
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOOD CH	1998	30700101
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOOD CH	1998	30700107
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOOD CH	1999	30700101
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOOD CH	1999	30700107
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOOD CH	2000	30700101

0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOOD CH	2000	30700107
0050009	PANAMA CITY MILL	30 WOODYARD FACILITY	1996	30700801
0050009	PANAMA CITY MILL	30 WOODYARD FACILITY	1997	30700801
0050009	PANAMA CITY MILL	30 WOODYARD FACILITY	1998	30700801
0050009	PANAMA CITY MILL	30 WOODYARD FACILITY	1999	30700801
0050009	PANAMA CITY MILL	30 WOODYARD FACILITY	2000	30700801
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1996	40700815
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1996	40700816
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1997	40700815
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1998	40700815
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1998	40700816
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1999	40700815
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1999	40700816
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	2000	40700815
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	2000	40700816
0050009	PANAMA CITY MILL	32 Papermaking/Warehouse	1999	
0050009	PANAMA CITY MILL	32 Papermaking/Warehouse	2000	30700401
0050009	PANAMA CITY MILL	33 Bleach plant with wet scrubber	1999	
0050009	PANAMA CITY MILL	33 Bleach plant with wet scrubber	2000	30700114

USAGE RATE	UNIT
294732	Tons Air-dried Unbleached Pulp
347709	Tons Air-dried Unbleached Pulp
860.2	1000 Gallons Burned
36.02	Million Cubic Feet Burned
228917	Tons Air-dried Unbleached Pulp
1124.7	1000 Gallons Burned
53.3	Million Cubic Feet Burned
333626	Tons Air-dried Unbleached Pulp
1491.5	1000 Gallons Burned
36.6	Million Cubic Feet Burned
284375	Tons Air-dried Unbleached Pulp
606445	Tons Air-dried Unbleached Pulp
689231	Tons Air-dried Unbleached Pulp
445364	Tons Air-dried Unbleached Pulp
4211.68	1000 Gallons Burned
119.77	Million Cubic Feet Burned
667877	Tons Air-dried Unbleached Pulp
7045	1000 Gallons Burned
109.7	Million Cubic Feet Burned
601216	Tons Air-dried Unbleached Pulp
5219	1000 Gallons Burned
302.8	Million Cubic Feet Burned
606445	Tons Air-dried Unbleached Pulp
689231	Tons Air-dried Unbleached Pulp
445364	Tons Air-dried Unbleached Pulp
667877	Tons Air-dried Unbleached Pulp
601216	Tons Air-dried Unbleached Pulp
3323.12	1000 Gallons Burned
106.94	Million Cubic Feet Burned
586	Tons Burned
3443.5	1000 Gallons Burned
97.21	Million Cubic Feet Burned
149362	Tons Burned
3179.4	1000 Gallons Burned
80.37	Million Cubic Feet Burned
138872	Tons Burned
4735	1000 Gallons Burned
84.1	Million Cubic Feet Burned
206210	Tons Burned
2716	1000 Gallons Burned
57.8	Million Cubic Feet Burned
0	Million Cubic Feet Burned
203989	Tons Burned
60421	Tons Burned
3563.3	1000 Gallons Burned
160.02	Million Cubic Feet Burned
173396	Tons Burned

77610	Tons Burned
1344	1000 Gallons Burned
145.47	Million Cubic Feet Burned
122203	Tons Burned
39475	Tons Burned
2656.6	1000 Gallons Burned
120.26	Million Cubic Feet Burned
127580	Tons Burned
51741	Tons Burned
4015.5	1000 Gallons Burned
60.9	Million Cubic Feet Burned
111036	Tons Burned
66450	Tons Burned
904.7	1000 Gallons Burned
47.1	Million Cubic Feet Burned
135992	Tons Burned
311713	Tons Air-dried Unbleached Pulp
343254	Tons Air-dried Unbleached Pulp
1002.92	1000 Gallons Burned
36.4	Million Cubic Feet Burned
216447	Tons Air-dried Unbleached Pulp
1052.94	1000 Gallons Burned
53.36	Million Cubic Feet Burned
334251	Tons Air-dried Unbleached Pulp
1581.3	1000 Gallons Burned
36.7	Million Cubic Feet Burned
316841	Tons Air-dried Unbleached Pulp
311713	Tons Air-dried Unbleached Pulp
341522	Tons Air-dried Unbleached Pulp
216447	Tons Air-dried Unbleached Pulp
334251	Tons Air-dried Unbleached Pulp
316841	Tons Air-dried Unbleached Pulp
294732	Tons Air-dried Unbleached Pulp
347709	Tons Air-dried Unbleached Pulp
228917	Tons Air-dried Unbleached Pulp
333626	Tons Air-dried Unbleached Pulp
284375	Tons Air-dried Unbleached Pulp
606445	Tons Air-dried Unbleached Pulp
689231	Tons Air-dried Unbleached Pulp
445364	Tons Air-dried Unbleached Pulp
667877	Tons Air-dried Unbleached Pulp
601216	Tons Air-dried Unbleached Pulp
606445	Tons Air-dried Unbleached Pulp
689231	Tons Air-dried Unbleached Pulp
445364	Tons Air-dried Unbleached Pulp
445364	Tons Air-dried Unbleached Pulp
667877	Tons Air-dried Unbleached Pulp
0	Tons Air-dried Unbleached Pulp
601216	Tons Air-dried Unbleached Pulp

0	Tons Air-dried Unbleached Pulp
2145956	Tons of Logs Processed
1275299	Tons of Logs Processed
858479	Tons of Logs Processed
1321282	Tons of Logs Processed
1222518	Tons of Logs Processed
230	1000 Gallons Storage Capacity
230	1000 Gallons Throughput
246	1000 Gallons Storage Capacity
184	1000 Gallons Storage Capacity
184	1000 Gallons Throughput
296.6	1000 Gallons Storage Capacity
0	1000 Gallons Throughput
247.9	1000 Gallons Storage Capacity
247.9	1000 Gallons Throughput
590194	Tons Finished Product
307794	Tons Air-dried Unbleached Pulp

Woodyard

① AC03-145859 — 8/16/88 elevated ent

roundwood: 355,118 cords/yr
purchased chips: 416,812 "

② 0050009-003-AE — 1/5/98

roundwood: 710,760 cords/yr
purchased chips: 609,840 "

NOW ③

roundwood: 1,946,954 cords/yr
purchased chips: 1,524,600

8/16/88 - present
Roundwood: 5.48 x ↑
Purchased Chips: 3.66 x ↑

Batch Digesters:

PN ① AC03-252285
7/5/94

22 new b.d.
5 blow tanks
1 accumulator tank

87.3 TPH ADUP

Not SN ② Amendment — 6/11/96 — 120 TPH ADUP

③ 0050009-002-AV
Est date: 6/28/2000

For PSD purposes, 120 TPH ADUP
668,850 TPY ADUP

SN ④ AC03-142979 — 10/26/88

For tissue, 79.6 TPH ADUP
For PSD purposes, 668,850 TPY ADUP
For NSPS and max. prod. / 120 TPH = 1911 TPD ADUP

Nos 3 + 4 Bark Boilers

No PM 1. AC03-190964 12/4/95. added to fuels of:

Primary clarified wood waste

of 10 TPD; c 2hr/w

?

No. 1 & No. 2 SDS

No PN

1. A003-222668 — 12-4-95 — the max. allowable op. rate is 123,700 lbs/hr BLS Std to RB No. 1

A003-240550

Lime kiln:

@ 12/4/95 — A003-174979 — max. process input rate 85,000 lb/hr lime mud (dry), based on a max. lime production of 36,720 lbs CaO dry

No PM annual letter

A003-174793 — max. allowable op. rate is 85,000 lb/hr lime mud (dry) input

NOTICE OF FINAL PERMIT

In the Matter of an
Application for Permit by:

Jack B. Prescott
General Manager
Stone Container Corporation
One Everitt Ave
Panama City FL 32402

FINAL Permit No.: 0050009-002-AV
Panama City Plant

_____/

Enclosed is FINAL Permit Number 0050009-002-AV for the operation of the Panama City Plant located at One Everitt Avenue, Panama City, Bay County, issued pursuant to Chapter 403, Florida Statutes (F.S.).

Any party to this order (permit) has the right to seek judicial review of it under Section 120.68 of the Florida Statutes, by the filing of a Notice of Appeal under Rule 9.110 of the Florida Rules of Appellate Procedure, with the clerk of the Department of Environmental Protection in the Office of General Counsel, 3900 Commonwealth Boulevard, Mail Station #35, Tallahassee, Florida, 32399-3000; and by filing a copy of the Notice of Appeal accompanied by the applicable filing fees with the appropriate District Court of Appeal. The Notice of Appeal must be filed within thirty days from the date this order is filed with the clerk of the permitting authority.

Executed in Pensacola, Florida.

FLORIDA DEPARTMENT OF
ENVIRONMENTAL PROTECTION

_____
Ed K. Middleswart, P.E.
Air Program Administrator
Northwest District

CERTIFICATE OF SERVICE

The undersigned duly designated deputy agency clerk hereby certifies that this NOTICE OF FINAL PERMIT (including the FINAL permit) was sent by certified mail (*) and copies were mailed by U.S. Mail before the close of business on _____ to the person(s) listed or as otherwise noted:

Mr. Jack B. Prescott, Stone Container Corp.*
Mr. Scott Sheplak, P.E., FDEP Bureau of Air Regulation
Ms. Gracy Danois, USEPA, Region 4 (INTERNET E-mail Memorandum)

FILING AND ACKNOWLEDGMENT FILED, on this date, pursuant to Section 120.52(7), Florida Statutes, with the designated agency Clerk, receipt of which is hereby acknowledged.

_____ _____
(Clerk) (Date)

Stone Container Corporation
Panama City Mill
Facility ID No.: 0050009
Bay County

Initial Title V Air Operation Permit
FINAL Permit No.: 0050009-002-AV

Permitting and Compliance Authority:
Department of Environmental Protection
Northwest District Office
160 Governmental Center
Pensacola, FL 32501-5794
Telephone: 850/595-8364
Fax: 850/595-8096

[electronic file name: 0330042f.doc]

Table of Contents

Permittee:
Stone Container Corporation

FINAL Permit No.: 0050009-002-AV
Facility ID No.: 0050009
SIC Nos.: 26, 2611
Project: Initial Title V Air Operation Permit

This permit is for the operation of the Panama City Mill. This facility is located at One Everitt Avenue, Panama City, Bay County; UTM Coordinates: Zone 16, 632.8 km East and 3335.1 km North; Latitude: 30° 08' 30" North and Longitude: 85° 37' 25" West.

STATEMENT OF BASIS: This Title V air operation permit is issued under the provisions of Chapter 403, Florida Statutes (F.S.) and Florida Administrative Code (F.A.C.) Chapters 62-4, 62-210, and 62-213. The above named permittee is hereby authorized to perform the work or operate the facility shown on the application and approved drawing(s), plans, and other documents, attached hereto or on file with the permitting authority, in accordance with the terms and conditions of this permit.

Referenced attachments made a part of this permit:
Appendix I-1, List of Insignificant Emissions Units and/or Activities
Appendix SS-1, Stack Sampling Facilities (version dated 10/07/96)
Appendix TV-3, Title V Conditions (version dated 04/30/99)
Appendix U-1, List of Unregulated Emissions Units and/or Activities
Table 297.310-1, Calibration Schedule (version dated 10/07/96)
TRS Contingency Plan

Effective Date: June 28, 2000
Renewal Application Due Date: January 1, 2005
Expiration Date: June 28, 2005

FLORIDA DEPARTMENT OF ENVIRONMENTAL PROTECTION

Ed K. Middleswart, P.E.
Air Program Administrator

EKM/rb

Section I. Facility Information.

Subsection A. Facility Description.

This facility is a Kraft pulp and paper mill that consists of major activities areas such as: wood handling facility, pulping, bleaching, chemical recovery, power house, paper machines, finishing/shipping/warehouse and associated processes and equipment.

Nos. 1 and 2 Recovery Boilers. Each recovery boiler is a direct contact recovery boiler with an electrostatic precipitator for particulate matter control. Each recovery boiler has a maximum heat input of 721 MMBtu/hr, which is equivalent to 123,700 pounds per hour of black liquor solids assuming 5,830 Btu/lb or black liquor solids. Black liquor either purchased or generated by the pulping process and containing between 5,200 and 6,300 Btu/lb is normally used for fuel but natural gas or No. 6 fuel oil with a maximum of 2.5% sulfur by weight may be used as a backup or supplemental fuel. Each boiler has a Koppers electrostatic precipitator with two sections of four fields each that controls particulate emissions. Total reduced sulfur emissions are monitored with a continuous emission monitor (CEM) system. These emissions units are regulated under Rule 62-296.404, F.A.C., Kraft Pulp Mills.

No. 3 Combination Boiler. The total maximum operational heat input of this emissions unit is 639 MMBtu/hr. The heat input is limited to 378 MMBtu/hr from fuel oil and 228 MMBtu/hr from carbonaceous fuels. This emissions unit may burn carbonaceous fuels (includes wood, bark and primary clarified wood fibers), natural gas and/or No. 2 or 6 fuel oil. Particulate emissions are controlled by a fly ash arrestor, model MTSA-380-9CVT, followed by a wet scrubber manufactured by FMC Link-Belt, model 200K dual-throat. Sulfur dioxide emissions are controlled by limiting the sulfur content of the fuel oil to a maximum of 2.4% by weight. This emissions unit is regulated under Rule 62-296.410, F.A.C., Carbonaceous Fuel Burning Equipment.

No. 4 Combination Boiler. The total maximum operational heat input of this emissions unit is 867 MMBtu/hr. The heat input is limited to 472 MMBtu/hr from fuel oil, 395 MMBtu/hr from coal and 273 MMBtu/hr from carbonaceous fuels. This emissions unit may burn carbonaceous fuels (includes wood, bark and primary clarified wood fibers), coal, natural gas and/or No. 2 or 6 fuel oil. Particulate emissions are controlled by a fly ash arrestor, model MTSA-380-9CVT, followed by a wet scrubber manufactured by FMC Link-Belt, model 200K dual-throat. Sulfur dioxide emissions are controlled when burning total reduced sulfur (TRS) gases and/or firing 100% fuel oil by maintaining a minimum pH of 8.0 in the wet scrubber (3-hour average). This boiler also serves as a backup control device for the non-condensable gases (NCG) from the Multiple-Effect Evaporator System and the Batch Digester System. TRS emissions are controlled by subjecting the TRS gases to a minimum of 1200°F for at least 0.5 seconds. This emissions unit is regulated under Rule 62-296.410, F.A.C., Carbonaceous Fuel Burning Equipment and Rule 62-296.404, F.A.C., Kraft Pulp Mills.

Nos. 1 and 2 Smelt Dissolving Tanks. The operating rate of each smelt dissolving tank is equal to the maximum allowed operating rate of each recovery boiler which is 123,700 pounds per hour of black liquor solids. The smelt is dissolved in weak wash to yield green liquor. Particulate emissions are controlled by demister pads manufactured by Munters Corporation. Total reduced sulfur emissions are controlled by weak wash sprays. The flow of the weak wash sprays is monitored as a surrogate compliance parameter. This emissions unit is regulated under Rule 62-296.404, F.A.C., Kraft Pulp Mills.

Lime Kiln. A natural gas or No. 6 fuel oil fired kiln with a maximum operating rate of 85,000 pounds per hour of lime mud. Maximum heat input to the kiln is 216 MMBtu per hour for natural gas and 139 MMBtu per hour for fuel oil. The kiln also serves as a control device for the NCG system. Particulate emissions are controlled by a venturi wet scrubber manufactured by Chemico, followed by a cyclone. Sulfur dioxide emissions are controlled by the sulfur content of the fuel oil (maximum of 2.5% by weight). Total reduced sulfur emissions are monitored with a CEM system. This emissions unit is regulated under Rule 62-296.404, F.A.C., Kraft Pulp Mills.

Methanol Storage Tank. A 38,500 gallon methanol vertical fixed roof storage tank with a flame arrestor. A nitrogen blanket flows over the methanol in the tank. The maximum annual throughput is 240,000 gallons per year. The storage tank and handling system are subject to recordkeeping and reporting requirements under the New Source Performance Standards (NSPS), 40 CFR 60, Subpart Kb.

Multiple Effect Evaporator (MEE) Systems. The evaporators are used to concentrate the weak black liquor prior to firing in the recovery furnaces. The total reduced sulfur emissions from the evaporators are collected by the NCG system and combusted in the lime kiln or No. 4 Bark Boiler. The maximum operating rate is 359,400 pounds of dry black liquor solids (BLS) per hour. Evaporator sets No. 1A, 2 and 3 process 208,000; 51,900; and 99,500 pounds of dry BLS/hr, respectively. This emissions unit is regulated under Rule 62-296.404, F.A.C., Kraft Pulp Mills.

Digester System. The digester system consists of twenty-two batch digesters, five blow tanks, one accumulator tank with both an upstream and downstream condenser, and a turpentine condensable system. The NCG handling system collects non-condensed gases containing total reduced sulfur compounds. Total reduced sulfur emissions are controlled by incineration in the lime kiln at 1200°F for at least 0.5 second, or in the No. 4 Bark Boiler as a backup. This emissions unit is regulated under Rule 62-296.404, F.A.C., and 40 CFR 60 Subpart BB, Kraft Pulp Mills.

Lime Slaker. Lime (CaO) from the lime kiln is added to green liquor (Na_2CO_3, Na_2S, and Na_2SO_4) in the slaker. The product of this reaction is white liquor (NaOH and Na_2S) used for cooking wood chips. Lime mud is formed as a byproduct which is recovered and regenerated to lime in the lime kiln. The maximum operating rate is 81.6 tons per hour of green liquor solids and lime (60.39 tph green liquor and 21.18 tph lime). Particulate emissions are controlled by a wet walled cyclone scrubber. This emissions unit is regulated under Rules 62-296.404, F.A.C., Kraft Pulp Mills and 62-296.320, F.A.C., General Pollutant Limiting Standards.

Woodyard. Wood chips are used as the raw material in the papermaking process and scrap wood and bark are used in steam generation. Roundwood (whole tree trunks) is received as either shortwood or longwood. Purchased hardwood or softwood chips are also received. Bark is a byproduct of log processing and some bark is also purchased. The chipping process begins by passing logs through a debarker to remove bark, which is collected and transferred via conveyors and hogged to obtain a desired size. After processing the bark, it is stored in piles, transferred to the bark bin, and then used as a fuel for the boilers at the facility. The logs are then chipped and the chips screened for proper size. Both purchased and manufactured chips are conveyed and stored in chip reclaimer storage piles. The facility has one softwood chip reclaimer and one hardwood reclaimer storage pile where chips are stored temporarily until needed by the facility. A single cyclone is associated with the bark transfer and conveying system, and used to pneumatically convey the bark. Conveyors are covered and roads are paved and maintained to minimize particulate entrainment. Four cyclones are used in the Screening Room to separate

pneumatically conveyed chips and fines from the conveying air stream. This emissions unit is regulated under Rule 62-296.320, F.A.C., General Pollutant Emission Limiting Standards.

Also included in this permit are miscellaneous insignificant and unregulated emissions units and/or activities.

Based on the initial Title V permit application received June 17, 1996, this facility is a major source of hazardous air pollutants (HAPs).

Subsection B. Summary of Emissions Unit ID No(s). and Brief Description(s).

E.U. ID No.	Brief Description
001	No. 1 Recovery Boiler
019	No. 2 Recovery Boiler
015	No. 3 Combination Boiler
016	No. 4 Combination Boiler
021	No. 1 Smelt Dissolving Tank
020	No. 2 Smelt Dissolving Tank
004	Lime Kiln
031	Methanol Storage Tank
026	Multiple Effect Evaporator Systems
027	Digester System, Non- Condensable Gas (NCG) Handling System
005	Lime Slaker
030	Woodyard
032	Unregulated Emissions Units (see Appendix U-1)

Please reference the Permit No., Facility ID No., and appropriate Emissions Unit(s) ID No(s). on all correspondence, test report submittals, applications, etc.

Subsection C. Relevant Documents.

The documents listed below are not a part of this permit; however, they are specifically related to this permitting action.

These documents are provided to the permittee for information purposes only:
Table 1-1, Summary of Air Pollutant Standards and Terms
Table 2-1, Summary of Compliance Requirements
Appendix A-1, Abbreviations, Acronyms, Citations, and Identification Numbers
Appendix H-1, Permit History / ID Number Changes

These documents are on file with permitting authority:
Initial Title V Permit Application received June 17, 1996

Section II. Facility-wide Conditions.

The following conditions apply facility-wide:

1. APPENDIX TV-3, TITLE V CONDITIONS, is a part of this permit.
{Permitting note: APPENDIX TV-3, TITLE V CONDITIONS, is distributed to the permittee only. Other persons requesting copies of these conditions shall be provided one copy when requested or otherwise appropriate.}

2. General Pollutant Emission Limiting Standards. Objectionable Odor Prohibited. The permittee shall not cause, suffer, allow, or permit the discharge of air pollutants which cause or contribute to an objectionable odor.
[Rule 62-296.320(2), F.A.C. and permit AC03-190964]

3. General Particulate Emission Limiting Standards. General Visible Emissions Standard. Except for emissions units that are subject to a particulate matter or opacity limit set forth or established by rule and reflected by conditions in this permit, no person shall cause, let, permit, suffer or allow to be discharged into the atmosphere the emissions of air pollutants from any activity, the density of which is equal to or greater than that designated as Number 1 on the Ringelmann Chart (20 percent opacity). EPA Method 9 is the method of compliance pursuant to Chapter 62-297, F.A.C. Visible emissions limits for kraft pulp mill emissions units equipped with wet scrubbers shall be effective only if the visible emission measurement can be made without being substantially affected by moisture condensation.
[Rules 62-296.320(4)(b)1. & 4. and 62-296.404(2)(b), F.A.C.]

4. Prevention of Accidental Releases (Section 112(r) of CAA).
a. As required by rule, inspection, or change in process the owner or operator shall submit an updated Risk Management Plan (RMP) to the Chemical Emergency Preparedness and Prevention Office (CEPPO) RMP Reporting Center.
b. The owner or operator shall report to the Department of Community Affairs (DCA) within one working day of discovery of an accidental release of a regulated substance from the stationary source, if the owner or operator is required to report the release to the USEPA/Chemical Safety Hazard Investigation Board or the National Response Center under Section 112(r)(6).
c. The owner or operator shall submit the required annual registration fee to the DCA on or before April 1 annually, in accordance with Part IV, Chapter 252, F.S. and Rule 9G-21, F.A.C.

5. Unregulated Emissions Units and/or Activities. Appendix U-1, List of Unregulated Emissions Units and/or Activities, is a part of this permit.
[Rule 62-213.440(1), F.A.C.]

6. Insignificant Emissions Units and/or Activities. Appendix I-1, List of Insignificant Emissions Units and/or Activities, is a part of this permit.
[Rules 62-213.440(1), 62-213.430(6), and 62-4.040(1)(b), F.A.C.]

7. General Pollutant Emission Limiting Standards. Volatile Organic Compounds (VOC) Emissions or Organic Solvents (OS) Emissions. The permittee shall allow no person to store, pump, handle, process, load, unload or use in any process or installation, volatile organic compounds (VOC) or organic solvents (OS) without applying known and existing vapor emission control devices or systems deemed necessary and ordered by the Department.
[Rule 62-296.320(1)(a), F.A.C.]

8. Reasonable precautions to prevent emissions of unconfined particulate matter at this facility include, but are not limited to, the application of water to stockpiles to control emissions and the implementation of good housekeeping practices.
[Rule 62-296.320(4)(c)2., F.A.C.; Proposed by applicant in the initial Title V permit application received June 17, 1996]

9. When appropriate, any recording, monitoring, or reporting requirements that are time-specific shall be in accordance with the effective date of the permit, which defines day one.
[Rule 62-213.440, F.A.C.]

10. The permittee shall submit all compliance related notifications and reports required of this permit to the Department's Northwest District office:

Department of Environmental Protection
Northwest District Office
160 Governmental Center
Pensacola, Florida 32501-5794
Telephone: 850/595-8364, press 7
Fax: 850/595-8096

11. Any reports, data, notifications, certifications, and requests required to be sent to the United States Environmental Protection Agency, Region 4, should be sent to:

United States Environmental Protection Agency
Region 4
Air, Pesticides & Toxics Management Division
Air and EPCRA Enforcement Branch, Air Enforcement Section
61 Forsyth Street
Atlanta, Georgia 30303
Telephone: 404/562-9055, Fax: 404/562-9164

12. The permittee shall comply with all the applicable standards and requirements of 40 CFR 63 Subpart S as specified in Attachment I (Amended Initial Notification Report, dated March 24, 2000), attached and incorporated by reference. The permittee shall comply with the reporting requirements of Subpart A of this part as specified in attachment Table 1. The Initial Notification Report shall be updated every two years and submitted to the Department for review.
[Rule 62-213.440(1), F.A.C., 40 CFR 63 Subpart S]

13. Statement of Compliance. The permittee shall submit a statement of compliance with all terms and conditions of the permit. {See condition 51., APPENDIX TV-3, TITLE V CONDITIONS}
[Rule 62-213.440(3), F.A.C.]

Section III. Emissions Units and Conditions.

Subsection A. This section addresses the following emissions units.

E.U. ID No.	Brief Description
001	No. 1 Direct Contact Recovery Boiler with an electrostatic precipitator for particulate control. TRS emissions are reduced by a two-stage heavy black liquor oxidation system.
019	No. 2 Direct Contact Recovery Boiler with an electrostatic precipitator for particulate control. TRS emissions are reduced by a two-stage heavy black liquor oxidation system.

This emissions unit is an existing source, not subject to NSPS or PSD.

The following specific conditions apply to the emissions units listed above:

Essential Potential to Emit (PTE) Parameters

A.1. Capacity. The maximum allowable operating rate of each boiler is 123,700 pounds of black liquor solids fired per hour based on a 24-hour average, as measured from the black liquor storage tanks and prior to each recovery boiler. {Permitting note: The capacity limitations have been placed in the permit to identify the capacity of each emissions unit for purposes of confirming that emissions testing is conducted within 90-100 percent of the emissions unit's rated capacity (or to limit future operation to 110 percent of the test load), to establish appropriate limits and to aid in determining future rule applicability.}
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

A.2. Methods of Operation - Fuels. The primary fuel shall be black liquor solids. Natural gas or No. 6 fuel oil with a maximum of 2.5% sulfur by weight may be used as a backup or supplemental fuel. Records of the sulfur content for each shipment of the fuel oil shall be maintained and available for inspection by the Department. The blending of fuel oil to achieve the sulfur standard is prohibited.
[Rules 62-4.160(2) and 62-213.440(1), F.A.C.]

A.3. Hours of Operation. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year.
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

Emission Limitations and Standards

{Permitting note: Table 1-1, Summary of Air Pollutant Standards and Terms, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

A.4. Particulate Matter. Particulate matter emissions from each unit shall not exceed 3 pounds per 3000 pounds of black liquor solids burned or 112.5 pounds per hour, whichever is less. The rate of black liquor solids fired shall be monitored and recorded continuously, and the records made available for Department inspection. {Permitting Note: The averaging time for this condition is based on the run time of the specified test method.}
[Rule 62-296.404(2)(a), F.A.C., and operating permits AO03-222669 and AO03-240555]

A.5. Visible Emissions. Visible emissions shall not exceed 45% opacity (6-minute average), except for up to 60% for one 6-minute period during any hour.
[Rules 62-296.404(1)(a), and 62-296.404(1)(a)1., F.A.C.]

A.6. Total Reduced Sulfur. Total reduced sulfur emissions from each unit shall not exceed 17.5 ppm by volume on a dry basis at standard conditions corrected to 8% oxygen as a 12-hour average.
[Rule 62-296.404(3)(c)1.a., F.A.C.]

Test Methods and Procedures

{Permitting note: Table 2-1, Summary of Compliance Requirements, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

A.7. Emissions Tests. See common condition number **K.1.**

A.8. Particulate Matter. The test method for particulate matter shall be EPA test method 5, incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rules 62-296.404(4)(a)2., and 62-297.401, F.A.C.]

A.9. Visible Emissions. The test method for visible emissions shall be EPA test method 9, incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rules 62-296.404(4)(a)1., and 62-297.401, F.A.C.]

A.10. Total Reduced Sulfur. The test method for total reduced sulfur shall be EPA test method 16, 16A or 16B incorporated and adopted by reference in Chapter 62-297, F.A.C. Testing is required only upon permit renewal.
[Rules 62-296.404(4)(a)3., and 62-297.401, F.A.C.]

Continuous Monitoring Requirements

A.11. Total Reduced Sulfur Continuous Monitoring. See common condition number **K.4.**

A.12. Quarterly Emission Reports. See common condition number **K.2.**

A.13. Determination of Process Variables. See common condition number **K.3.**

A.14. Excess Emissions. See common condition number **K.5.**

A.15. Periodic Monitoring. Until the requirements of MACT II are implemented, the permittee will maintain and monitor the existing opacity meters. Corrective action will be taken whenever the one hour average opacity exceeds 30%. Records of the opacity shall be maintained and available for inspection by the Department.
[Rule 62-213.440(4), F.A.C.]

Subsection B. This section addresses the following emissions unit.

E.U. ID No.	Brief Description
015	No. 3 Combination Boiler with particulate matter emissions controlled by a venturi scrubber.

This emissions unit is an existing source, not subject to NSPS or PSD.

The following specific conditions apply to the emissions unit listed above:

Essential Potential to Emit (PTE) Parameters

B.1. Capacity. The total maximum operational heat input of this emissions unit is 639 MMBtu/hr. The heat input shall not exceed 378 MMBtu/hr from fuel oil, 228 MMBtu/hr from carbonaceous fuels, or 33 MMBtu/hr from natural gas. {Permitting note: The capacity limitations have been placed in the permit to identify the capacity of each emissions unit for purposes of confirming that emissions testing is conducted within 90-100 percent of the emissions unit's rated capacity (or to limit future operation to 110 percent of the test load), to establish appropriate limits and to aid in determining future rule applicability.}
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

B.2. Methods of Operation - Fuels. This emissions unit may burn carbonaceous fuels (includes wood, bark and primary clarified wood fibers), natural gas and No. 2 or 6 fuel oil (maximum of 2.4% sulfur by weight). Records of the sulfur content for each shipment of the fuel oil shall be maintained and available for inspection by the Department. The blending of fuel oil to achieve the sulfur standard is prohibited. [Note: carbonaceous fuel consumption rates shall be expressed on a dry solids basis]
[Rules 62-4.160(2) and 62-213.440(1), F.A.C.]

B.3. Hours of Operation. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year.
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

Emission Limitations and Standards

{Permitting note: Table 1-1, Summary of Air Pollutant Standards and Terms, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

B.4. Particulate Matter. Particulate matter emissions shall not exceed 0.3 lb per MMBtu heat input from carbonaceous fuels or 0.1 lb per MMBtu heat input from natural gas and fuel oil. {Permitting Note: The averaging time for this condition is based on the run time of the specified test method.}
[Rule 62-296.410(1)(b)2., F.A.C.]

B.5. Visible Emissions. Visible emissions shall not exceed 30% opacity except for two minutes per hour of not more than 40% opacity.
[Rule 62-296.410(1)(b)1., F.A.C.]

Test Methods and Procedures

{Permitting note: Table 2-1, Summary of Compliance Requirements, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

B.6. Emissions Tests. See common condition number **K.1.**

B.7. Particulate Matter. The test method for particulate matter shall be EPA Method 5, incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rules 62-296.410(3)(b) and 62-297.401, F.A.C.]

B.8. Visible Emissions. The test method for visible emissions shall be EPA Method 9, incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rules 62-296.410(3)(a) and 62-297.401, F.A.C.]

Monitoring of Operations

B.9. Determination of Process Variables. See common condition number **K.3.**

B.10. Excess Emissions. See common condition number **K.5.**

B.11. Periodic Monitoring. Within six months of the effective date of this permit, the permittee shall install the necessary equipment to monitor either scrubber flow or differential pressure. The set point for this parameter will be established during the annual testing and is subject to Department approval. Hourly monitoring records shall be maintained and available for inspection by the Department.
[Rule 62-213.440(4), F.A.C.]

Subsection C. This section addresses the following emissions unit.

E.U. ID No.	Brief Description
016	No. 4 Combination Boiler with particulate matter emissions controlled by a wet scrubber. As a backup to the lime kiln, NCGs from the batch digesting system and multiple effects evaporator system are transported to this boiler for incineration of TRS.

This emissions unit is an existing source, not subject to NSPS or PSD.

The following specific conditions apply to the emissions unit listed above:

Essential Potential to Emit (PTE) Parameters

C.1. Capacity. The total maximum operational heat input of this emissions unit is 867 MMBtu/hr. The heat input shall not exceed 472 MMBtu/hr from fuel oil, 395 MMBtu/hr from coal, 273 MMBtu/hr from carbonaceous fuels, or 40 MMBtu/hr from natural gas. Capacity records shall be maintained and available for inspection by the Department.
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C. and construction permit AC03-190964]

C.2. Methods of Operation - Fuels. This emissions unit may burn carbonaceous fuels (includes wood, bark and primary clarified wood fibers), coal (maximum of 1.7% sulfur by weight), natural gas and No. 2 or 6 fuel oil (maximum of 2.4% sulfur by weight). Records of the sulfur content for each shipment of fuel oil and coal shall be maintained and available for inspection by the Department. The blending of fuel oil to achieve the sulfur standard is prohibited. [Note: carbonaceous fuel consumption rates shall be expressed on a dry solids basis]
[Rules 62-4.160(2) and 62-213.440(1), F.A.C.]

C.3. Hours of Operation. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year.
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

Emission Limitations and Standards

{Permitting note: Table 1-1, Summary of Air Pollutant Standards and Terms, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

C.4. Particulate Matter. Particulate matter emissions shall not exceed 0.1 pound per MMBtu of heat input or 86.7 pounds per hour from fossil fuel firing, and 0.3 pound per MMBtu heat input or 81.9 pounds per hour from carbonaceous fuels. {Permitting Note: The averaging time for this condition is based on the run time of the specified test method.}
[Rule 62-296.410(1)(b)2, F.A.C.]

C.5. Sulfur Dioxide. Sulfur dioxide emissions shall not exceed 781 pounds per hour when incinerating TRS gases, and 772 pounds per hour when not incinerating TRS gases.
[Construction Permit AC03-190964]

C.6. Visible Emissions. Visible emissions shall not exceed 30% opacity except for two minutes period per hour of not more than 40% opacity.
[Rule 62-296.410(1)(b)1., F.A.C.]

C.7. Total Reduced Sulfur. Total reduced sulfur emissions shall not exceed 5 ppm by volume on a dry basis at standard conditions corrected to 10% oxygen as a 12 hour average.
[Rule 62-296.404(3)(f)1., F.A.C.]

Test Methods and Procedures

{Permitting note: Table 2-1, Summary of Compliance Requirements, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

C.8. Emissions Tests. See common condition number **K.1.**

C.9. Particulate Matter. The test method for particulate matter shall be EPA Method 5, incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rules 62-296.410(3)(b) and 62-297.401, F.A.C.]

C.10. Sulfur Dioxide. The test method for SO2 shall be EPA Method 6, incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Construction Permit AC03-190964 and Rule 62-297.401, F.A.C.]

C.11. Visible Emissions. The test method for visible emissions shall be EPA Method 9, incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rules 62-296.410(3)(a) and 62-297.401, F.A.C.]

C.12. Total Reduced Sulfur. The test method for total reduced sulfur shall be EPA Method 16, 16A or 16B incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rule 62-297.404(4)(b)3. and 62-297.401, F.A.C.]

Monitoring of Operations

C.13. Total Reduced Sulfur. When TRS gases are collected and transported to this boiler for incineration, the TRS gases shall be subject to a minimum of 1200 degrees F for at least 0.5 seconds. Temperature and oxygen shall be monitored and recorded continuously, and the records made available for Department inspection. The temperature devices shall be certified by the manufacturer to be accurate to within ±1 percent of the temperature being measured. The oxygen monitors shall be certified by the manufacturer to be accurate to within 0.1 percent oxygen by volume.
[Rule 62-296.404(5)(c), F.A.C., and Construction Permit AC03-190964]

C.14. Sulfur dioxide emissions shall be controlled, when firing 100% fuel oil and/or incinerating TRS gases, by maintaining the pH of the venturi scrubber scrubbing medium above 8.0. Compliance shall be based upon a three-hour average. The pH shall be monitored and recorded continuously, and the records made available for Department inspection. The set point for this parameter will be re-evaluated during the annual testing and is subject to Department approval.
[Construction Permit AC03-190964]

C.15. Quarterly Emission Reports. See common condition number **K.2.**

C.16. Determination of Process Variables. See common condition number **K.3.**

C.17. Excess Emissions. See common condition number **K.5.**

C.18. Periodic Monitoring. Within six months of the effective date of this permit, the permittee shall install the necessary equipment to monitor either scrubber flow or differential pressure. The set point for this parameter will be established during the annual testing and is subject to Department approval. Hourly monitoring records shall be maintained and available for inspection by the Department.
[Rule 62-213.440(4), F.A.C.]

Subsection D. This section addresses the following emissions units.

E.U. ID No.	Brief Description
021	No. 1 Smelt Dissolving Tank with a mist eliminator and stack sprays to control emissions.
020	No. 2 Smelt Dissolving Tank with a mist eliminator and stack sprays to control emissions.

This emissions unit is an existing source, not subject to NSPS or PSD.

The following specific conditions apply to the emissions units listed above:

Essential Potential to Emit (PTE) Parameters

D.1. Capacity. The maximum operating rate of each unit is 123,700 pounds of black liquor solids per hour fired in its respective recovery furnace. Records of the black liquor solids throughput for each smelt dissolving tank shall be maintained and available for inspection by the Department. {Permitting note: The capacity limitations have been placed in the permit to identify the capacity of each emissions unit for purposes of confirming that emissions testing is conducted within 90-100 percent of the emissions unit's rated capacity (or to limit future operation to 110 percent of the test load), to establish appropriate limits and to aid in determining future rule applicability.}
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

D.2. Hours of Operation. These emissions units are allowed to operate continuously, i.e., 8,760 hours/year.
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

Emission Limitations and Standards

{Permitting note: Table 1-1, Summary of Air Pollutant Standards and Terms, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

D.3. Particulate Matter. Particulate matter from each unit shall not exceed 29 pounds per hour at the maximum operating rate, nor that allowed by the process weight table.
[Rule 62-296.320(4)(a), F.A.C.]

D.4. Total Reduced Sulfur. Total reduced sulfur from each unit shall not exceed 0.048 pounds per 3000 pounds of black liquor solids as hydrogen sulfide (12-hour average).
[Rule 62-296.404(3)(d)1., F.A.C.]

D.5. Visible Emissions. Visible emissions shall not exceed 20% opacity. If observed greater than 20% opacity by the Department, a special compliance test may be required to demonstrate compliance with the particulate matter mass emissions standard.
[Rule 62-296.404(2)(b), F.A.C.]

Test Methods and Procedures

{Permitting note: Table 2-1, Summary of Compliance Requirements, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

D.6. Emissions Tests. See common condition number **K.1.**

D.7. Particulate Matter. The test method for particulate matter shall be EPA Method 5, incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rules 62-296.404(4)(c)1. and 62-297.401, F.A.C.]

D.8. Total Reduced Sulfur. The test method for total reduced sulfur shall be EPA test method 16, 16A or 16B incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rules 62-296.404(4)(c)3. and 62-297.401, F.A.C.]

D.9. Visible Emissions. The test method for visible emissions shall be EPA Method 9, incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rule 62-297.401, F.A.C.]

Monitoring of Operations

D.10. Total Reduced Sulfur. Compliance with the TRS standard shall be demonstrated by maintaining the pre-demister weak wash injection fluid at a minimum of 20 and 40.8 gallons per minute based on a 12-hour average for No. 1 and No. 2 smelt dissolving tank, respectively. Flow rates shall be checked and recorded hourly and the records maintained and made available for inspection by the Department. The set point for this parameter will be re-evaluated during the annual testing and is subject to Department approval. All 12-hour averages below the set points will be reported as excess emissions as outlined in D.11., below.
[Rule 62-296.404(3)(d)2., F.A.C.]

D.11. Quarterly Emission Reports. See common condition number **K.2.**

D.12. Determination of Process Variables. See common condition number **K.3.**

D.13. Excess Emissions. See common condition number **K.5.**

Subsection E. This section addresses the following emissions unit.

E.U. ID No.	Brief Description
004	Lime Kiln with a venturi scrubber to control particulate matter emissions.

This emissions unit is an existing source, not subject to NSPS or PSD.

The following specific conditions apply to the emissions unit listed above:

Essential Potential to Emit (PTE) Parameters

E.1. Capacity. The maximum allowable operating rate is 85,000 pounds per hour of lime mud input, dry basis (24-hour average), based on a maximum lime production of 36,700 lbs CaO/hr dry. Capacity records shall be maintained and available for inspection by the Department.
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C., and Construction Permit AC03-149719]

E.2. Methods of Operation - Fuels. This emission unit shall be fueled by natural gas or number 6 fuel oil with a maximum sulfur content of 2.5 %, by weight. Records of the sulfur content of each shipment of fuel oil shall be maintained and available for inspection by the Department. The No. 6 fuel oil or natural gas firing rate shall not exceed 139 MMBtu or 216 MMBtu per hour heat input, respectively. The blending of fuel oil to achieve the sulfur standard is prohibited.
[Rules 62-4.160(2) and 62-213.440(1), F.A.C.]

E.3. Hours of Operation. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year.
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

Emission Limitations and Standards

{Permitting note: Table 1-1, Summary of Air Pollutant Standards and Terms, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

E.4. Particulate Matter. Particulate matter emissions from this unit shall not exceed 29.83 pounds per hour, nor that allowed by the process weight table.
[Rule 62-296.320(4)(a), F.A.C., and construction permit AC03-149719]

E.5. Total Reduced Sulfur. Total reduced sulfur emissions shall not exceed 20 ppm by volume on a dry basis at standard conditions corrected to 10% oxygen as a 12-hour average.
[Rule 62-296.404(3)(e)1, F.A.C.]

E.6. Visible Emissions. Visible emissions shall not exceed 20% opacity. If observed greater than 20% opacity by the Department, a special compliance test may be required to demonstrate compliance with the particulate matter mass emissions standard.
[Rule 62-296.404(2)(b), F.A.C.]

Test Methods and Procedures

{Permitting note: Table 2-1, Summary of Compliance Requirements, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

E.7. Emissions Tests. See common condition number **K.1.**

E.8. Particulate Matter. The test method for particulate matter shall be EPA test method 5, incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rules 62-296.404(4)(b)1., and 62-297.401, F.A.C.]

E.9. Total Reduced Sulfur. The test method for total reduced sulfur shall be EPA test method 16, 16A, or 16B incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rules 62-296.404(4)(b)3., and 62-297.401, F.A.C.]

E.10. Visible Emissions. The test method for visible emissions shall be EPA test method 9, incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rule 62-297.401, F.A.C.]

Continuous Monitoring Requirements

E.11. Total Reduced Sulfur Continuous Monitoring. See common condition number **K.4.**

E.12. Quarterly Emission Reports. See common condition number **K.2.**

E.13. Determination of Process Variables. See common condition number **K.3.**

E.14. Excess Emissions. See common condition number **K.5.**

E.15. Periodic Monitoring. The scrubber flow shall be maintained at a minimum of 800 gallons per minute, 190 gallons per minute minimum scrubber recirculation flow and a minimum differential pressure of 18 inches of water. The set point for these parameters will be re-evaluated during the annual testing and is subject to Department approval. Hourly records of the flow and pressure differential shall be maintained and available for inspection by the Department.
[Rule 62-213.440(4), F.A.C.]

Subsection F. This section addresses the following emissions units.

E.U. ID No.	Brief Description
031	38,500 gallon fixed-roof, nitrogen blanketed, methanol storage tank

This emissions unit is a new source, subject to NSPS but not PSD.

The following specific conditions apply to the emissions unit listed above:

Essential Potential to Emit (PTE) Parameters

F.1. Capacity. This emissions unit has a 38,500 gallon storage capacity. Maximum annual throughput is 240,000 gallons per year. {Permitting note: The capacity limitations have been placed in the permit to identify the capacity of each emissions unit for purposes of confirming that emissions testing is conducted within 90-100 percent of the emissions unit's rated capacity (or to limit future operation to 110 percent of the test load), to establish appropriate limits and to aid in determining future rule applicability.}
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

F.2. NSPS Provisions. The owner or operator of this storage vessel shall keep readily accessible records showing the dimension of the storage vessel and an analysis showing the capacity of the storage vessel for the life of the source. Records of the VOL stored, the period of storage, and the maximum true vapor pressure of that VOL during the respective storage period shall be maintained for a period of five years.
[Rule 62-204.800(7)(b)16., F.A.C., and 40CFR 60.116(b)]

F.3. Hours of Operation. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year.
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

Subsection G. This section addresses the following emissions unit.

E.U. ID No.	Brief Description
026	Nos. 1A, 2 and 3 Multiple Effect Evaporator (MEE) Sets

This emissions unit is an existing source, not subject to NSPS or PSD.

The following specific conditions apply to the emissions unit listed above:

Essential Potential to Emit (PTE) Parameters

G.1. Capacity. The maximum process input rate is 359,400 pounds of dry black liquor solids per hour to the MEE system. (Evaporator sets No. 1A, No. 2, and No. 3 process 208,000; 51,900; and 99,500 pounds of dry BLS/hr, respectively). Capacity records shall be maintained and available for inspection by the Department.

[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C. and construction permits AC03-149716, AC03-149717 and AC03-149718]

G.2. Hours of Operation. This emissions unit is allowed to operate continuously, i.e., 8760 hours/year.
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

Emission Limitations and Standards

{Permitting note: Table 1-1, Summary of Air Pollutant Standards and Terms, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

G.3. Total Reduced Sulfur. The TRS emissions from the MEE Systems shall be collected and incinerated in the Lime Kiln or the No. 4 Combination Boiler. Malfunctions resulting in uncontrolled TRS emissions from the MEE Systems shall be managed in accordance with the facility's TRS Venting Contingency Plan attached to and made a part of this permit.
[Rule 62-4.404(3)(a), F.A.C.]

G.4. A log of NCG ventings to the atmosphere shall be maintained and available for inspection by the Department. The log shall include but not be limited to the date and time, duration, cause and corrective actions taken for each venting occurrence. In no event shall the cumulative venting time exceed ten days in any annual period. Each venting occurrence shall be reported to the Department verbally by the next working day and a copy of the log entry submitted within 30 days.
[Rule 62-4.404(3)(a), F.A.C.]

FINAL Permit No.: 0050009-002-AV

Subsection H. This section addresses the following emissions units.

E.U. ID No.	Brief Description
027	Digester System, Non- Condensable Gas (NCG) Handling System

This emissions unit is a new source, subject to NSPS but not PSD.

The following specific conditions apply to the emissions unit(s) listed above:

Essential Potential to Emit (PTE) Parameters

H.1. Capacity. For PSD purposes, the maximum allowable operating rate is 120 tons of air dried unbleached pulp (ADUP) per hour and a maximum production rate of 668,850 tons per years of ADUP. Capacity records shall be maintained and available for inspection by the Department.
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C. and construction permit AC03-252285]

H.2. Hours of Operation. This emissions unit is allowed to operate continuously, i.e., 8760 hours/year.
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

Emission Limitations and Standards

{Permitting note: Table 1-1, Summary of Air Pollutant Standards and Terms, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

H.3. Non-Condensible Gases (NCGs). The NCGs from the batch digesters, blow tanks, accumulator tank, and turpentine condenser system shall be destroyed in the lime kiln or the No. 4 Combination boiler by subjecting the TRS gases to at least 1200°F for at least 0.5 seconds. Malfunctions shall be handled in accordance with the facility's TRS Venting Contingency Plan attached to and made a part of this permit.
[Rules 62-204.800(7)(b)35., and 62-296.404(3)(a)1., F.A.C.]

Monitoring of Operations

H.4. A log of NCG ventings to the atmosphere shall be maintained and available for inspection by the Department. The log shall include but not limited to the date and time, duration, cause and corrective actions taken for each venting occurrence. In no event shall the cumulative venting time exceed ten days in any annual period.
[Rules 62-204.800(7)(b)35., and 62-296.404(3)(a)3., F.A.C.]

H.5. Determination of Process Variables. See common condition number **K.3.**

Subsection I. This section addresses the following emissions unit.

E.U. ID No.	Brief Description
005	Lime Slaker with a wet cyclonic scrubber to control particulate matter emissions.

This emissions unit is an existing source, not subject to NSPS or PSD.

The following specific conditions apply to the emissions unit listed above:

Essential Potential to Emit (PTE) Parameters

I.1. Capacity. The maximum operating rate is 81.6 tons per hour (60.39 tph green liquor and 21.18 tph lime. {Permitting note: The capacity limitations have been placed in the permit to identify the capacity of each emissions unit for purposes of confirming that emissions testing is conducted within 90-100 percent of the emissions unit's rated capacity (or to limit future operation to 110 percent of the test load), to establish appropriate limits and to aid in determining future rule applicability.}
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

I.2. Hours of Operation. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year.
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

Emission Limitations and Standards

{Permitting note: Table 1-1, Summary of Air Pollutant Standards and Terms, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

I.3. Particulate Matter. Particulate matter shall not exceed 32.3 pounds per hour, nor that allowed by the process weight table.
[Rule 62-296.320(4)(a), F.A.C.]

I.4. Visible Emissions. Visible emissions shall not exceed 20% opacity. If observed greater than 20% opacity by the Department, a special compliance test may be required to demonstrate compliance with the particulate matter mass emissions standard.
[Rule 62-296.404(2)(b), F.A.C.]

Test Methods and Procedures

{Permitting note: Table 2-1, Summary of Compliance Requirements, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

I.5. Emissions Tests. See common condition number **K.1.** Compliance tests are required upon permit renewal.
[Rule 62-297.310, F.A.C.]

I.6. Particulate Matter. The test method shall be EPA Method 5, incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rule 62-296.320(4)(a) and 62-297.401, F.A.C.]

I.7. Visible Emissions. The test method for visible emissions shall be EPA test method 9, incorporated and adopted by reference in Chapter 62-297, F.A.C.
[Rule 62-297.401, F.A.C.]

Continuous Monitoring Requirements

I.8. The weak wash flow to the scrubber shall not be less than 30 gallons per minute. The flow shall be monitored and recorded continuously and the records made available to the Department for inspection. The set point for this parameter will be re-evaluated during the annual testing and is subject to Department approval.
[Rule 62-4.160(2), F.A.C., and Permit AO03-252354]

I.9. Determination of Process Variables. See common condition number **K.3.**

I.10. Excess Emissions. See common condition number **K.5.**

Subsection J. This section addresses the following emissions units.

E.U. ID No.	Brief Description
030	Woodyard

This emissions unit is an existing source, not subject to NSPS or PSD.

The following specific conditions apply to the emissions units listed above:

Essential Potential to Emit (PTE) Parameters

J.1. Capacity. The maximum operation rate of this emissions unit is 710,160 cords/year of roundwood and 609,840 cords/year of purchased chips. Operation records shall be maintained and available for inspection by the Department.
[Rules 62-4.160(2), 62-210.200(PTE), F.A.C. and permit 0050009-003-AC]

J.2. Hours of Operation. This emissions unit is allowed to operate continuously, i.e., 8,760 hours/year.
[Rules 62-4.160(2) and 62-210.200(PTE), F.A.C.]

Emission Limitations and Standards

{Permitting note: Table 1-1, Summary of Air Pollutant Standards and Terms, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

J.3. Visible Emissions Visible emissions shall not exceed 20% opacity.
[Rule 62-296.320(4)(b)1., F.A.C.]

J.4. Reasonable precautions shall be taken to prevent emissions of unconfined particulate matter. Reasonable precautions shall include, but are not limited to, the following:

a. Maintenance of roads, parking areas and yards.
b. Application of water or other dust suppressants when necessary to control emissions.
c. Removal of particulate matter from roads and other paved areas under control of the owner or operator, and from buildings or work areas to prevent re-entrainment.
d. Permittee will protect dust transfer points and transport and storage containers from wind action which might make dust airborne.
e. Chips manufactured on-site shall be screened following storage.
f. Chips will be screened following removal from storage prior to conveying to digesters.
g. All conveyor systems shall be covered or enclosed.
h. Drop distance from chip storage stacker shall be maintained to a minimum.
i. All access roads shall be paved.

[Rule 62-296.320(4)(c), F.A.C., and Construction Permit 0050009-003-AC]

Test Methods and Procedures

{Permitting note: Table 2-1, Summary of Compliance Requirements, summarizes information for convenience purposes only. This table does not supersede any of the terms or conditions of this permit.}

J.5. Visible Emissions testing shall be performed upon request by the Department. [Rule 62-204.800(7)(b)1., F.A.C.]

J.6. Visible Emissions. The test method for visible emissions shall be EPA test method 9, incorporated and adopted by reference in Chapter 62-297, F.A.C. [Rule 62-297.401, F.A.C.]

J.7. Determination of Process Variables. See common condition number **K.3.**

J.8. Excess Emissions. See common condition number **K.5.**

Subsection K. Common Conditions.

{Permitting Note: The following conditions are placed here as a convenience and to avoid duplication. See specific conditions in Subsections A through J for applicability.}

K.1. Test Methods and Procedures

Emissions tests are required to show continuing compliance with the standards of the Department. The test results must provide reasonable assurance that the source is capable of compliance at the permitted maximum operating rate. Tests shall be conducted annually, unless otherwise specified in Sections III.A. through III.J. Results shall be submitted to the Department within 45 days after testing. The Department shall be notified at least 15 days prior to testing to allow witnessing.
[Rule 62-297.310, F.A.C.]

Testing of emissions shall be conducted with the emissions unit operating at permitted capacity, which is defined as 90 to 100 percent of the maximum operation rate allowed by the permit. If it is impracticable to test at permitted capacity, an emissions unit may be tested at less than the minimum permitted capacity (i.e., at less than 90 percent of the maximum operation rate allowed by the permit); in this case, subsequent emissions unit operation is limited to 110 percent of the test load until a new test is conducted, provided however, operations do not exceed 100 percent of the maximum operation rate allowed by the permit. Once the emissions unit is so limited, operation at higher capacities is allowed for no more than 15 consecutive days for the purpose of additional compliance testing to regain the authority to operate at the permitted capacity.
[Rules 62-297.310(2) & (2)b., F.A.C.]

K.2. Quarterly Reporting Requirements.

The permittee shall submit a quarterly written report of emissions in excess of any emission limiting standards.

(a) The report shall include the following information:

1. The magnitude of excess emissions and the date and time of commencement and completion of each time period in which excess emissions occurred.

2. Specific identification of each period of excess emissions that occurs including startups, shutdowns, and malfunctions of the affected emissions unit. An explanation of the cause of each period of excess emissions, and any corrective action taken or preventive measures adopted.

3. The date and time identifying each period during which each continuous emissions monitoring system was inoperative except for zero and span checks, and the nature of the system repairs or adjustments.

4. When no excess emissions have occurred or the continuous emissions monitoring system(s) have not been operative, or have been repaired or adjusted, such information shall be stated in the report.

(b) Any owner or operator shall maintain a complete file of any measurements, including continuous emissions monitoring system, monitoring device, and performance testing measurements; any continuous emissions monitoring system performance evaluations; any continuous emissions monitoring system or monitoring device calibration checks; any adjustments and maintenance performed on these systems or devices; and any other information required, recorded in a permanent legible form available for inspection.
[Rules 62-296.405(1)(g), 62-296.404(6), and 62-204.800(7), F.A.C.]

K.3. Determination of Process Variables.

The owner or operator of an emissions unit for which compliance tests are required shall install, operate, and maintain equipment or instruments necessary to determine process variables, such as process weight input or heat input, when such data are needed in conjunction with emissions data to determine the compliance of the emissions unit with applicable emission limiting standards.

Equipment or instruments used to directly or indirectly determine process variables, including devices such as belt scales, weight hoppers, flow meters, and tank scales, shall be calibrated and adjusted to indicate the true value of the parameter being measured with sufficient accuracy to allow the applicable process variable to be determined within 10% of its true value.
[Rule 62-297.310(5), F.A.C.]

K.4. Total Reduced Sulfur Continuous Emissions Monitoring Requirements.

The permittee shall maintain a continuous monitoring system for monitoring total reduced sulfur (TRS) emissions. The TRS continuous emissions monitoring system shall be installed, calibrated, certified and operated pursuant to all of the following provisions:

a. The continuous emissions monitoring system shall monitor and record the concentration of total reduced sulfur (TRS) emissions on a dry basis and the percentage of oxygen by volume on a dry basis.

b. The continuous emissions monitoring system shall complete a minimum of one cycle of operation (sampling, analyzing, and data recording) for each successive 15-minute period.

c. The continuous emissions monitoring system shall be located downstream of the control device such that representative measurements of process parameters can be obtained.

d. The continuous emissions monitoring system shall be located, installed and certified pursuant to the provisions of 40 CFR Part 60, Appendix B, Performance Specification 2 and Performance Specification 3, and 40 CFR Part 60, Appendix B, Performance Specification 5, which are adopted by reference in Rule 62-204.800(7), F.A.C. The exception is that the phrase "or other approved alternative" in s. 3.2 of Performance Specification 5 is not adopted. For the purposes of compliance testing and certification of continuous emissions monitoring systems, 40 CFR Part 60, Appendix A, Reference Method 16 and Method 16A, adopted by reference in Rule 62-204.800(7), F.A.C., are to be used.

e. The continuous emissions monitoring system shall be in continuous operation, except when the emissions unit is not operating, or during system breakdowns, repairs, calibration checks, and zero and span adjustments.

f. During any initial compliance tests conducted pursuant to Rule 62-296.404, F.A.C., or within 30 days thereafter, and at such times as there is reason to believe the system does not conform to the performance specifications under this rule (for example, equipment repairs, replacements, excessive drift and such), the owner or operator of any affected emissions unit shall conduct continuous monitoring system performance evaluations and furnish the Department, within sixty days thereof, two copies of a written report of the results of such tests. These continuous emissions monitoring systems performance evaluations shall be conducted in accordance with the requirements and procedures contained in Rule 62-296.404(5)(b)1.d., F.A.C.

g. The continuous emissions monitoring system shall have a maximum span value not to exceed:

(i) A total reduced sulfur concentration of 30 ppm for the total reduced sulfur continuous emissions monitoring system on any new design direct-fired kraft recovery furnace that is not direct-fired, new design suspension-burning kraft recovery furnace, incinerator, digester system or multiple effect evaporator system.

(ii) A total reduced sulfur concentration of 50 ppm for the total reduced sulfur continuous emissions monitoring system on any old design kraft recovery furnace, new design kraft recovery furnace that is not direct-fired, new design direct-fired suspension-burning kraft recovery furnace, cross recovery furnace, lime kiln or calciner.

(iii) 20 percent oxygen for the continuous oxygen monitoring system.

h. The continuous emissions monitoring system shall be checked by the owner or operator in accordance with a written procedure at least once daily and after any maintenance to the system. The owner or operator shall check the zero (or low level value between 0 and 20 percent of span value) and span (90 to 100 percent of span value) calibration drifts. The zero and span shall be adjusted, as a minimum, whenever the 24-hour zero drift or 24-hour span drift exceeds two times the limits of the applicable performance specifications referenced in Rule 62-296.404(5)(b)1.d., F.A.C. The system must allow the amount of excess zero and span drift measured at the 24-hour interval checks to be recorded and quantified.
[Rule 62-296.404(5), F.A.C.]

K.5. Excess Emissions.

(1) Excess emissions resulting from startup, shutdown or malfunction of any emissions unit shall be permitted providing (1) best operational practices to minimize emissions are adhered to and (2) the duration of excess emissions shall be minimized but in no case exceed two hours in any 24 hour period unless specifically authorized by the Department for longer duration.

(2) Excess emissions from existing fossil fuel steam generators resulting from startup or shutdown shall be permitted provided that best operational practices to minimize emissions are adhered to and the duration of excess emissions shall be minimized.

(3) Excess emissions from existing fossil fuel steam generators resulting from boiler cleaning (soot blowing) and load change shall be permitted provided the duration of such excess emissions shall not exceed 3 hours in any 24-hour period and visible emissions shall not exceed Number 3 of the Ringelmann Chart (60 percent opacity), and providing (1) best operational practices to minimize emissions are adhered to and (2) the duration of excess emissions shall be minimized.

A load change occurs when the operational capacity of a unit is in the 10 percent to 100 percent capacity range, other than startup or shutdown, which exceeds 10 percent of the unit's rated capacity and which occurs at a rate of 0.5 percent per minute or more.

Visible emissions above 60 percent opacity shall be allowed for not more than 4, six (6)-minute periods, during the 3-hour period of excess emissions allowed by this subparagraph, for boiler cleaning and load changes, at units which have installed and are operating, or have committed to install or operate, continuous opacity monitors.

Particulate matter emissions shall not exceed an average of 0.3 lbs. per million BTU heat input during the 3-hour period of excess emissions allowed by this subparagraph.

(4) Excess emissions which are caused entirely or in part by poor maintenance, poor operation, or any other equipment or process failure which may reasonably be prevented during startup, shutdown, or malfunction shall be prohibited.

(5) Considering operational variations in types of industrial equipment operations affected by this rule, the Department may adjust maximum and minimum factors to provide reasonable and practical regulatory controls consistent with the public interest.

(6) In case of excess emissions resulting from malfunctions, each owner or operator shall notify the Department or the appropriate Local Program in accordance with Rule 62-4.130, F.A.C. A full written report on the malfunctions shall be submitted in a quarterly report, if requested by the Department.

The requirements of this rule do not vary any requirement of a NSPS, NESHAP, or Acid Rain program provision.
[Rule 62-210.700, F.A.C.]

Department of Environmental Protection

Lawton Chiles
Governor

Northwest District
160 Governmental Center
Pensacola, Florida 32501-5794

Virginia B. Wetherell
Secretary

PERMITTEE:

Stone Container Corporation

I.D. Number: 10PCY03000927
Permit/Certification Number: AC03-252285
Date of Issue: July 5, 1994
Expiration Date: June 15, 1995
County: Bay
Latitude/Longitude:30°08'30"N/85°37'25"W
Project: Digester System Rebuild

This permit is issued under the provisions of section 403.087,Florida Statutes, and Florida Administrative Code Rules 17-296, 17-297 and 17-4. The above named applicant, hereinafter called permittee, is hereby authorized to perform the work or operate the facility shown on the application and approved drawings, plans, and other documents attached hereto or on file with the Department and made a part hereof and specifically described as follows:

The 22 digester systems will be replaced in kind and the emissions will be totally contained in the existing NCG collection system and routed to the lime kiln for incineration. The No. 4 Bark Boiler serves as backup to the lime kiln for TRS incineration. The TRS gases will be subjected to a minimum temperature of 1200 degrees Fahrenheit for at least 0.5 seconds in either of the two combustion devices. The 22 batch digester systems consist of five blow tanks, one accumulator tank with a condenser before and after the accumulator tank and a turpentine condensing system following the accumulator. The maximum process rate will not increase as a result of the new digester system.

The project is located at the permittee's kraft pulp mill in Panama City, Bay County, Florida. The UTM coordinates are zone 16, 632.8 km East, and 3335.1 km North.

The Standard Industrial Codes are:
Industry No. 2611-Pulp Mills
~~Industry No. 2621-Paper Mills~~

The Standard Classification Codes are:
Pulp and Paper Industry Major Group 26:
Sulfate (Kraft) Pulping
BATCH DIGESTER SYSTEM 3-07-001-01
TERPENE CONDENSER 3-07-001-07

PERMITTEE:

Stone Container Corporation

I.D. Number: 10PCY03000927
Permit/Certification Number: AC03-252285
Date of Issue: July 5, 1994
Expiration Date: June 15, 1995

SPECIFIC CONDITIONS:

General

1. The attached General Conditions are part of this permit. [FAC Rule 17-4.160]

Construction

2. The Department shall be notified upon initial commissioning of the new Digester system. [FAC Rule 17-4.210]

3. The Department shall be notified and prior approval obtained of any changes or revisions from the June 6, 1994 application. [FAC Rule 17-4.210]

Operation

4. The digester system may operate continuously (8760 hours per year). [FAC Rule 17-4.070]

5. The maximum production rate will be 87.3 tons per hour air dried unbleached pulp (ADUP). [FAC Rule 17-4.070]

6. The non-condensible gases (NCG) from the batch digesters, blow tanks, accumulator tank and turpentine condenser system shall be destroyed in the Lime Kiln or the Bark Boiler by subjecting the TRS gases to at least 1200°F for at least 0.5 seconds. [FAC Rule 17-296.404(3)(e)]

7. The digester system is subject to the total reduced sulfur (TRS) emission limiting standard which requires combustion of the TRS gases in the lime kiln. [FAC Rule 17-296.404(3)(a)1]

Administrative

8. Submit an updated TRS VENTING CONTINGENCY PLAN with the request for the operation permit. The plan shall include definitions of what constitutes a reportable venting incident and an assessment of the use of the back-up control device.[17-296.404(3)3]

9. The new process equipment shall be installed in such a manner to facilitate regular inspections and maintenance to minimize fugitive gaseous emissions. [FAC Rule 17-4.070]

10. An annual operation report shall be submitted by March 1 each year. [FAC Rule 17-210.370]

11. A major air pollution source Annual Operation Fee Form must be completed and submitted with the appropriate fee between January 15 and March 1 of each year.[FAC Rule 17-213]

Post-it® Fax Note 7671	Date 4/30/02 # of pages ▶ 10
To BRUCE MITCHELL	From RICK BRADBURN
Co./Dept. DARM	Co. NWD AIR
Phone #	Phone # SC 695 8364
Fax # SC 292-6979	Fax # X1233

To: Andy Allen
From: Bob Kriegel
Date: June 6, 1996

Re: **Letter Request from Stone Container, Bay County to change Permitted Production Rates; EMU ID no. 0050009027, permit no. AO03-270940**

By letter dated May 24, 1996 KBN requested that Stone Container Corporation permits AO03-270940 and AC03-252285 be changed by increasing the maximum production of the batch digester system from 87.3 TPH ADUP to 120 TPH and including a maximum daily pulp production rate of 2,096.3 TPD ADUP. KBN noted that these changes were consistent with the original permit which identified a pulp production capacity of 120 TPH, and that the monthly averaged, daily limit would insure no increase in air emissions. As such Stone requests that language in SC 15 of the construction permit, and SC 2 of the operation permit be changed as follows:

FROM:

AC03-252285:

SC 5: The maximum production rate will be 87.3 tons per hour air dried unbleached pulp (ADUP).

AO03-270940:

SC 2: The maximum allowable operating rate is 87.3 tons per hour air dried unbleached pulp (ADUP) per hour.

TO:

The maximum allowable operating rate is 120 tons per hour air dried unbleached pulp (ADUP), and 2096.3 tons per day ADUP (monthly average).

Permit AC03-142979 was issued September 24, 1989 by DARM and identified a maximum production rate of 120 tons ADUP per hour and 1911 tons of ADUP per day. This permit identified the maximum production rate for testing purposes to 79.6 tons of ADUP per hour. Subsequently permit AO03-174790 was issued August 10, 1990; and, specific condition 15 limited the maximum production of the digester systems to 120 tons ADUP per hour, but for testing purposes limited production of the digester system to 79.6 tons ADUP per hour.

Construction permit AC03-252285 was issued July 5, 1994 allowing replacement of the 22 digester systems; and, included a condition limiting the maximum production rate to 87.3 tons per hour ADUP. The application (see page ATT-2) identifies maximum

Stone Container Corporation
North American Containerboard,
Paper and Pulp Division

Panama City Mill

Post Office Box 2560
Panama City, Florida 32402

(904) 785-4311

May 10, 1995

RECEIVED

MAY 16 1995

Northwest Florida
DEP

Mr. Ed Middleswart, P.E.
Air Resource Management
Department of Environmental Protection
160 Governmental Center
Pensacola, Florida 32501-5794

Dear Mr. Middleswart:

Enclosed are four (4) copies of an operating permit application for the digester system at the Panama City Mill of Stone Container Corporation. Also enclosed is a TRS venting contingency plan.

If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Yours truly,

L.D. Riley, Jr.
Environmental Superintendent

LDR/mw
cc: J. Prescott/C. Bogatie (w/o encl.)
David Buff - KBN Engineering

Emissions Unit Information Section 1 of 1

Emissions Unit Control Equipment

1. Description: Incineration of TRS gases in the lime kiln (No. 4 Bark Boiler is backup)
2. Control Device or Method Code(s): 022

Emissions Unit Operating Capacity

1. Maximum Heat Input Rate:	mmBtu/hr	
2. Maximum Incineration Rate:	lb/hr	tons/day
3. Maximum Process or Throughput Rate:		
4. Maximum Production Rate: 87.3 TPH air dried unbleached pulp		
5. Operating Capacity Comment:		

Emissions Unit Operating Schedule

Requested Maximum Operating Schedule:			
24	hours/day	7	days/week
52	weeks/year	8,760	hours/year

per A0003-174790; limit 120 tons (ADUB)/hr
test purposes - 79.6

CP Order - 78.6 ADUP/hr

Stone Container Corporation

Containerboard and Paper Division

Panama City Mill

Post Office Box 2560
Panama City, Florida 32402

(904) 785 4311

May 16, 1994

Mr. Ed Middleswart, P.E.
Air Resources Management
Department of Environmental Protection
160 Governmental Center
Pensacola, FL 32501-5794

Dear Mr. Middleswart:

On April 13, we had a catastrophic failure of a batch digester at the Panama City Mill of Stone Container Corporation. Because of the extensive damage caused by the failure and the age of the remaining undamaged digesters (16 of 22), it has been determined that the most prudent course of action is to replace all the digesters at this time.

The digesters will be replaced in kind; therefore, there will be no production increase because of this project. Noncondensable gasses from the new digesters and the turpentine recovery system will be collected in the existing NCG collection and incineration system just as the gasses from the old digester system were. The NCG collecting system was not damaged by the failure; therefore, repairs and alterations to this system are not necessary.

It is our opinion that this project does not require permitting for the following reasons:

1. The digesters are being replace in kind and in the identical location of the old digesters.

2. There will be no production increase resulting from this project.

3. The existing air emissions control system will be used for the new digesters.

4. There will be no increase in air or water pollutants.

Please confirm your concurrence with this opinion to us in writing.

Stone Container Corporation

Containerboard and Paper Division

Panama City Mill

Post Office Box 2560
Panama City, Florida 32402

(904) 785-4311

June 3, 1994

Mr. Ed Middleswart, P.E.
Air Resource Management
Department of Environmental Regulation
160 Governmental Center
Pensacola, Florida 32501-5794

Dear Mr. Middleswart:

Enclosed are four copies of the construction permit applications to install the replacement digesters at the Panama City Mill of Stone Container Corporation. Please note that these digesters are identical replacements for the digesters being removed from service because of the catastrophic failure we experienced in April, 1994. Also note that the existing NCG system will be used for TRS control, since it was not damaged by the explosion.

If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Sincerely yours,

L.D. Riley, Jr.
Environmental Superintendent

RECEIVED
JUN - 6 1994
Northwest Florida
DEP

/mkd

cc: Jack B. Prescott

If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Yours truly,

L. D. Riley, Jr.

L. D. Riley, Jr.
Environmental Superintendent

/mkd

CC: Jack Prescott

ATTACHMENT A

1.0 PROCESS DESCRIPTION

Stone Container Corporation (SCC) owns and operates a kraft pulp mill located in Panama City, Florida. The facility includes twenty-two (22) batch digesters which are used to cook wood chips to produce pulp for the paper and linerboard making process. The location of the mill in relation to the surrounding area is shown in Figure 1. A plot plan of the mill is presented in Figure 2.

Recently, a catastrophic accident took place at the mill involving the batch digester system. One of the digester structures failed, resulting in severe damage to the digester as well as several other digesters. After careful study, SCC has decided to replace all of the batch digesters at the mill, in order to reduce the potential for further digester structure failures.

The existing batch digester system is permitted under Florida Department of Environmental Protection (FDEP) operating permit AO03-174790 issued on August 10, 1990. The maximum permitted production rate of the system is 120 tons per hour (TPH) of air dried unbleached pulp (ADUP).

A flow diagram of the digester system which is now in operation at SCC is shown in Figure 3. The arrangement of the 22 batch digesters and blow tanks is shown in Figure 4.

As shown in Figures 3 and 4, the batch digester system at SCC consists of 22 batch digesters, five (5) blow tanks, and one (1) accumulator tank. Condensers are located before and after the accumulator tank in order to collect condensibles from the gas/vapor stream. A turpentine condensing system also follows the accumulator in order to recover turpentine from the system.

Although each of the 22 batch digesters is essentially identical, eight (8) are designated to produce primary pulp, twelve (12) are designated to produce easy bleached kraft (EBK) pulp, and two (2) are designated to produce secondary pulp. The system is arranged such that the two secondary pulp digesters discharge to the No. 1 Blow Tank. Three of the primary digesters can discharge to either the No. 1 Blow Tank or the No. 2 Blow Tank. Two other primary digesters discharge only to the No. 2 Blow Tank. The remaining three primary digesters discharge to the No. 4 Blow Tank.

Of the twelve EBK digesters, one can discharge to either the No. 3 or No. 4 Blow Tank, five discharge only to the No. 3 Blow tank, and six discharge only to the No. 5 Blow Tank.

As shown in Figure 3, non-condensible gases (NCG) from the batch digesters, blow tanks, accumulator tank and turpentine condenser system are collected and sent to the Lime Kiln at the facility for destruction of total reduced sulfur (TRS). The No. 4 Bark Boiler is used as a backup destruction device.

SCC is proposing to replace all twenty two of the existing batch digesters. However, the remainder of the batch digester system, including the NCG incineration system, will not be replaced or modified. Each of the new digesters will be approximately 2,600 cubic feet in size. The maximum process rate of the digester system will not increase as a result of these changes.

2.0 DERIVATION OF PROCESS INPUT RATES

The future maximum input of raw materials to the digesters and the maximum product weights are based upon the following:

Maximum 24-hour pulp production:

= 1,886.7 TPD, dry basis

= 157,225 lb/hr, dry basis, 24-hour maximum. = 78.6 TPH pulp.

EBK Pulp (12 digesters)

Raw material inputs per digester per blow:

31.25 tons wood chips = 62,500 lbs

6,500 gal white liquor @ 9.9 lb/gal = 64,350 lbs

3,000 gal weak black liquor @ 8.6 lb/gal = 25,800 lbs

Total input per blow = 62,500 + 64,350 + 25,800 = 152,650 lbs

Maximum blows per day = 120 total for 12 digesters

Blows per hour = 5

Total raw material input:

Wood chips = 62,500 lbs/blow x 5 blows/hr = 312,500 lbs/hr

White liquor = 64,350 lbs/blow x 5 blows/hr = 321,750 lbs/hr

Weak black liquor = 25,800 lbs/blow x 5 blows/day = 129,000 lbs/hr

Total = 312,500 + 321,750 + 129,000 = 763,250 lbs/hr

Primary Pulp (8 digesters)

Raw material inputs per digester per blow:

31.25 tons wood chips = 62,500 lbs

3,500 gal white liquor @ 9.9 lb/gal = 34,650 lbs

5,000 gal weak black liquor @ 8.6 lb/gal = 43,000 lbs

Total input per blow = 62,500 + 34,650 + 43,000 = 140,150 lbs

Maximum blows per day = 95 total for 8 digesters

Blows per hour = 4

Total raw material input:

Wood chips = 62,500 lbs/blow x 4 blows/hr = 250,000 lbs/hr

White liquor = 34,650 lbs/blow x 4 blows/hr = 138,600 lbs/hr

Weak black liquor = 43,000 lbs/blow x 4 blows/day = 172,000 lbs/hr

Total = 250,000 + 138,600 + 172,000 = 560,600 lbs/hr

Secondary Pulp (2 digesters)

Raw material inputs per digester per blow:

31.25 tons wood chips = 62,500 lbs

5,000 gal white liquor @ 9.9 lb/gal = 49,500 lbs

3,500 gal weak black liquor @ 8.6 lb/gal = 30,100 lbs

Total input per blow = 62,500 + 49,500 + 30,100 = 142,100 lbs

Maximum blows per day = 16 total for 2 digesters

Blows per hour = 0.67

Total raw material input:

Wood chips = 62,500 lbs/blow x 0.67 blows/hr = 41,875 lbs/hr

White liquor = 49,500 lbs/blow x 0.67 blows/hr = 33,165 lbs/hr

Weak black liquor = 30,100 lbs/blow x 0.67 blows/day = 20,167 lbs/hr

Total = 41,875 + 33,165 + 20,167 = 95,207 lbs/hr

Total Process Input Rate For All Digesters

Total process input rate = EBK + Primary + Secondary pulp

Total wood chips: 312,500 + 250,000 + 41,875 = 604,375 lbs/hr

Total white liquor = 321,750 + 138,600 + 33,165 = 493,515 lbs/hr

Total weak black liquor = 129,000 + 172,000 + 20,167 = 321,167 lbs/hr

Total = 604,375 + 493,515 + 321,167 = 1,418,709 lb/hr

3.0 TRS EMISSION ESTIMATES

TRS emission estimates are based upon TRS emission factors published in EPA Publication AP-42. The emission factor is based on tons of air dried unbleached pulp (ADUP), which contains approximately 10 percent moisture.

1,886.7 TPD dry pulp ÷ (1 - 0.1) = 2,096.3 TPD ADUP

TRS emissions = 2,096.3 TPD ADUP x 1.2 lb/ton ADUP ÷ 24 hr/day

= 104.8 lb/hr TRS

2,096.3 TPD ADUP x 1.2 lb/ton x 365 days/yr ÷ 2,000 lb/ton = 459.1 TPY

The TRS emissions from the digester system are controlled by venting the gases to the lime kiln or the No. 4 Bark Boiler for incineration. The TRS gases will be subject to a temperature of at least 1,200°F for at least 0.5 seconds in either of these combustion devices.

Department of Environmental Protection

Lawton Chiles
Governor

Northwest District
160 Governmental Center
Pensacola, Florida 32501-5794

Virginia B. Wetherell
Secretary

PERMITTEE:

Stone Container Corporation

I.D. Number: 10PCY03000927
Permit/Certification Number: AC03-252285
Date of Issue: July 5, 1994
Expiration Date: June 15, 1995
County: Bay
Latitude/Longitude:30°08'30"N/85°37'25"W
Project: Digester System Rebuild

This permit is issued under the provisions of section 403.087,Florida Statutes, and Florida Administrative Code Rules 17-296, 17-297 and 17-4. The above named applicant, hereinafter called permittee, is hereby authorized to perform the work or operate the facility shown on the application and approved drawings, plans, and other documents attached hereto or on file with the Department and made a part hereof and specifically described as follows:

The 22 digester systems will be replaced in kind and the emissions will be totally contained in the existing NCG collection system and routed to the lime kiln for incineration. The No. 4 Bark Boiler serves as backup to the lime kiln for TRS incineration. The TRS gases will be subjected to a minimum temperature of 1200 degrees Fahrenheit for at least 0.5 seconds in either of the two combustion devices. The 22 batch digester systems consist of five blow tanks, one accumulator tank with a condenser before and after the accumulator tank and a turpentine condensing system following the accumulator. The maximum process rate will not increase as a result of the new digester system.

The project is located at the permittee's kraft pulp mill in Panama City, Bay County, Florida. The UTM coordinates are zone 16, 632.8 km East, and 3335.1 km North.

The Standard Industrial Codes are:
Industry No. 2611-Pulp Mills
~~Industry No. 2621-Paper Mills~~

The Standard Classification Codes are:
Pulp and Paper Industry Major Group 26:
Sulfate (Kraft) Pulping
BATCH DIGESTER SYSTEM 3-07-001-01
TERPENE CONDENSER 3-07-001-07

PERMITTEE:

Stone Container Corporation

I.D. Number: 10PCY03000927
Permit/Certification Number: AC03-252285
Date of Issue: July 5, 1994
Expiration Date: June 15, 1995

SPECIFIC CONDITIONS:

General

1. The attached General Conditions are part of this permit. [FAC Rule 17-4.160]

Construction

2. The Department shall be notified upon initial commissioning of the new Digester system. [FAC Rule 17-4.210]

3. The Department shall be notified and prior approval obtained of any changes or revisions from the June 6, 1994 application. [FAC Rule 17-4.210]

Operation

4. The digester system may operate continuously (8760 hours per year). [FAC Rule 17-4.070]

5. The maximum production rate will be 87.3 tons per hour air dried unbleached pulp (ADUP). [FAC Rule 17-4.070]

6. The non-condensible gases (NCG) from the batch digesters, blow tanks, accumulator tank and turpentine condenser system shall be destroyed in the Lime Kiln or the Bark Boiler by subjecting the TRS gases to at least 1200°F for at least 0.5 seconds. [FAC Rule 17-296.404(3)(e)]

7. The digester system is subject to the total reduced sulfur (TRS) emission limiting standard which requires combustion of the TRS gases in the lime kiln. [FAC Rule 17-296.404(3)(a)1]

Administrative

8. Submit an updated TRS VENTING CONTINGENCY PLAN with the request for the operation permit. The plan shall include definitions of what constitutes a reportable venting incident and an assessment of the use of the back-up control device.[17-296.404(3)3]

9. The new process equipment shall be installed in such a manner to facilitate regular inspections and maintenance to minimize fugitive gaseous emissions. [FAC Rule 17-4.070]

10. An annual operation report shall be submitted by March 1 each year. [FAC Rule 17-210.370]

11. A major air pollution source Annual Operation Fee Form must be completed and submitted with the appropriate fee between January 15 and March 1 of each year.[FAC Rule 17-213]

Stone Container Corporation
North American Containerboard,
Paper and Pulp Division

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(904) 785-4311

May 10, 1995

Mr. Ed Middleswart, P.E.
Air Resource Management
Department of Environmental Protection
160 Governmental Center
Pensacola, Florida 32501-5794

Dear Mr. Middleswart:

Enclosed are four (4) copies of an operating permit application for the digester system at the Panama City Mill of Stone Container Corporation. Also enclosed is a TRS venting contingency plan.

If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Yours truly,

L.D. Riley, Jr.
Environmental Superintendent

LDR/mw
cc: J. Prescott/C. Bogatie (w/o encl.)
David Buff - KBN Engineering

Emissions Unit Information Section 1 of 1

Emissions Unit Control Equipment

1. Description: Incineration of TRS gases in the lime kiln (No. 4 Bark Boiler is backup)
2. Control Device or Method Code(s): 022

Emissions Unit Operating Capacity

1. Maximum Heat Input Rate:	mmBtu/hr	
2. Maximum Incineration Rate:	lb/hr	tons/day
3. Maximum Process or Throughput Rate:		
4. Maximum Production Rate: 87.3 TPH air dried unbleached pulp		
5. Operating Capacity Comment:		

Emissions Unit Operating Schedule

Requested Maximum Operating Schedule:			
24	hours/day	7	days/week
52	weeks/year	8,760	hours/year

per AO03-174790; limit 120 tons (ADUB)/hr
test purposes - 79.6

CP typo - 78.6 ADUP/hr

Post-it® Fax Note 7671	Date 4/30/02	# of pages ▶ 10
To BRUCE MITCHELL	From RICK BRADBURN	
Co./Dept. DARM	Co. NWD AIR	
Phone #	Phone # SC 695 8364	
Fax # SC 292-6979	Fax # X1233	

To: Andy Allen
From: Bob Kriegel
Date: June 6, 1996

Re: **Letter Request from Stone Container, Bay County to change Permitted Production Rates; EMU ID no. 0050009027, permit no. AO03-270940**

By letter dated May 24, 1996 KBN requested that Stone Container Corporation permits AO03-270940 and AC03-252285 be changed by increasing the maximum production of the batch digester system from 87.3 TPH ADUP to 120 TPH and including a maximum daily pulp production rate of 2,096.3 TPD ADUP. KBN noted that these changes were consistent with the original permit which identified a pulp production capacity of 120 TPH, and that the monthly averaged, daily limit would insure no increase in air emissions. As such Stone requests that language in SC 15 of the construction permit, and SC 2 of the operation permit be changed as follows:

FROM:

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SC 5: The maximum production rate will be 87.3 tons per hour air dried unbleached pulp (ADUP).

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SC 2: The maximum allowable operating rate is 87.3 tons per hour air dried unbleached pulp (ADUP) per hour.

TO:

The maximum allowable operating rate is 120 tons per hour air dried unbleached pulp (ADUP), and 2096.3 tons per day ADUP (monthly average).

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May 10, 1995

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MAY 16 1995

Northwest Florida
DEP

Mr. Ed Middleswart, P.E.
Air Resource Management
Department of Environmental Protection
160 Governmental Center
Pensacola, Florida 32501-5794

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If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Yours truly,

L.D. Riley, Jr.
Environmental Superintendent

LDR/mw
cc: J. Prescott/C. Bogatie (w/o encl.)
David Buff - KBN Engineering

Emissions Unit Information Section 1 of 1

Emissions Unit Control Equipment

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5. Operating Capacity Comment:		

Emissions Unit Operating Schedule

Requested Maximum Operating Schedule:			
	24 hours/day	7 days/week	
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permit AO03-174790; limit 120 tons (ADUB)/hr
test purposes - 79.6

CP Application - 78.6 ADUP/hr

Stone Container Corporation

Containerboard and Paper Division

Panama City Mill

Post Office Box 2560
Panama City, Florida 32402

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May 16, 1994

Mr. Ed Middleswart, P.E.
Air Resources Management
Department of Environmental Protection
160 Governmental Center
Pensacola, FL 32501-5794

Dear Mr. Middleswart:

On April 13, we had a catastrophic failure of a batch digester at the Panama City Mill of Stone Container Corporation. Because of the extensive damage caused by the failure and the age of the remaining undamaged digesters (16 of 22), it has been determined that the most prudent course of action is to replace all the digesters at this time.

The digesters will be replaced in kind; therefore, there will be no production increase because of this project. Noncondensable gasses from the new digesters and the turpentine recovery system will be collected in the existing NCG collection and incineration system just as the gasses from the old digester system were. The NCG collecting system was not damaged by the failure; therefore, repairs and alterations to this system are not necessary.

It is our opinion that this project does not require permitting for the following reasons:

1. The digesters are being replace in kind and in the identical location of the old digesters.

2. There will be no production increase resulting from this project.

3. The existing air emissions control system will be used for the new digesters.

4. There will be no increase in air or water pollutants.

Please confirm your concurrence with this opinion to us in writing.

Stone Container Corporation

Containerboard and Paper Division

Panama City Mill

Post Office Box 2560
Panama City, Florida 32402

(904) 785-4311

June 3, 1994

Gdm
6/6

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Air Resource Management
Department of Environmental Regulation
160 Governmental Center
Pensacola, Florida 32501-5794

Dear Mr. Middleswart:

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Sincerely yours,

L.D. Riley, Jr.
Environmental Superintendent

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/mkd

cc: Jack B. Prescott

If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Yours truly,

L. D. Riley, Jr.

L. D. Riley, Jr.
Environmental Superintendent

/mkd

CC: Jack Prescott

ATTACHMENT A

1.0 PROCESS DESCRIPTION

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Recently, a catastrophic accident took place at the mill involving the batch digester system. One of the digester structures failed, resulting in severe damage to the digester as well as several other digesters. After careful study, SCC has decided to replace all of the batch digesters at the mill, in order to reduce the potential for further digester structure failures.

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A flow diagram of the digester system which is now in operation at SCC is shown in Figure 3. The arrangement of the 22 batch digesters and blow tanks is shown in Figure 4.

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Although each of the 22 batch digesters is essentially identical, eight (8) are designated to produce primary pulp, twelve (12) are designated to produce easy bleached kraft (EBK) pulp, and two (2) are designated to produce secondary pulp. The system is arranged such that the two secondary pulp digesters discharge to the No. 1 Blow Tank. Three of the primary digesters can discharge to either the No. 1 Blow Tank or the No. 2 Blow Tank. Two other primary digesters discharge only to the No. 2 Blow Tank. The remaining three primary digesters discharge to the No. 4 Blow Tank.

Of the twelve EBK digesters, one can discharge to either the No. 3 or No. 4 Blow Tank, five discharge only to the No. 3 Blow tank, and six discharge only to the No. 5 Blow Tank.

As shown in Figure 3, non-condensible gases (NCG) from the batch digesters, blow tanks, accumulator tank and turpentine condenser system are collected and sent to the Lime Kiln at the facility for destruction of total reduced sulfur (TRS). The No. 4 Bark Boiler is used as a backup destruction device.

SCC is proposing to replace all twenty two of the existing batch digesters. However, the remainder of the batch digester system, including the NCG incineration system, will not be replaced or modified. Each of the new digesters will be approximately 2,600 cubic feet in size. The maximum process rate of the digester system will not increase as a result of these changes.

2.0 DERIVATION OF PROCESS INPUT RATES

The future maximum input of raw materials to the digesters and the maximum product weights are based upon the following:

Maximum 24-hour pulp production:

= 1,886.7 TPD, dry basis

= 157,225 lb/hr, dry basis, 24-hour maximum. ≈ 78.6 TPH pulp

EBK Pulp (12 digesters)

Raw material inputs per digester per blow:

31.25 tons wood chips = 62,500 lbs

6,500 gal white liquor @ 9.9 lb/gal = 64,350 lbs

3,000 gal weak black liquor @ 8.6 lb/gal = 25,800 lbs

Total input per blow = 62,500 + 64,350 + 25,800 = 152,650 lbs

Maximum blows per day = 120 total for 12 digesters

Blows per hour = 5

Total raw material input:

Wood chips = 62,500 lbs/blow x 5 blows/hr = 312,500 lbs/hr

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Primary Pulp (8 digesters)

Raw material inputs per digester per blow:

31.25 tons wood chips = 62,500 lbs

3,500 gal white liquor @ 9.9 lb/gal = 34,650 lbs

5,000 gal weak black liquor @ 8.6 lb/gal = 43,000 lbs

Total input per blow = 62,500 + 34,650 + 43,000 = 140,150 lbs

Maximum blows per day = 95 total for 8 digesters

Blows per hour = 4

Total raw material input:

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White liquor = 34,650 lbs/blow x 4 blows/hr = 138,600 lbs/hr

Weak black liquor = 43,000 lbs/blow x 4 blows/day = 172,000 lbs/hr

Total = 250,000 + 138,600 + 172,000 = 560,600 lbs/hr

Secondary Pulp (2 digesters)

Raw material inputs per digester per blow:

31.25 tons wood chips = 62,500 lbs

5,000 gal white liquor @ 9.9 lb/gal = 49,500 lbs

3,500 gal weak black liquor @ 8.6 lb/gal = 30,100 lbs

Total input per blow = 62,500 + 49,500 + 30,100 = 142,100 lbs

Maximum blows per day = 16 total for 2 digesters

Blows per hour = 0.67

Total raw material input:

Wood chips = 62,500 lbs/blow x 0.67 blows/hr = 41,875 lbs/hr

White liquor = 49,500 lbs/blow x 0.67 blows/hr = 33,165 lbs/hr

Weak black liquor = 30,100 lbs/blow x 0.67 blows/day = 20,167 lbs/hr

Total = 41,875 + 33,165 + 20,167 = 95,207 lbs/hr

Total Process Input Rate For All Digesters

Total process input rate = EBK + Primary + Secondary pulp

Total wood chips: 312,500 + 250,000 + 41,875 = 604,375 lbs/hr

Total white liquor = 321,750 + 138,600 + 33,165 = 493,515 lbs/hr

Total weak black liquor = 129,000 + 172,000 + 20,167 = 321,167 lbs/hr

Total = 604,375 + 493,515 + 321,167 = 1,418,709 lb/hr

3.0 TRS EMISSION ESTIMATES

TRS emission estimates are based upon TRS emission factors published in EPA Publication AP-42. The emission factor is based on tons of air dried unbleached pulp (ADUP), which contains approximately 10 percent moisture.

1,886.7 TPD dry pulp ÷ (1 - 0.1) = 2,096.3 TPD ADUP

TRS emissions = 2,096.3 TPD ADUP x 1.2 lb/ton ADUP ÷ 24 hr/day

= 104.8 lb/hr TRS

2,096.3 TPD ADUP x 1.2 lb/ton x 365 days/yr ÷ 2,000 lb/ton = 459.1 TPY

The TRS emissions from the digester system are controlled by venting the gases to the lime kiln or the No. 4 Bark Boiler for incineration. The TRS gases will be subject to a temperature of at least 1,200°F for at least 0.5 seconds in either of these combustion devices.

Post-it® Fax Note 7671	Date 4/30/02 # of pages ▶ 10
To BRUCE MITCHELL	From RICK BRADBURN
Co./Dept. DARM	Co. NWD AIR
Phone #	Phone # SC 695 8364
Fax # SC 292-6979	Fax # x1233

To: Andy Allen
From: Bob Krieger
Date: June 6, 1996

Re: **Letter Request from Stone Container, Bay County to change Permitted Production Rates; EMU ID no. 0050009027, permit no. AO03-270940**

By letter dated May 24, 1996 KBN requested that Stone Container Corporation permits AO03-270940 and AC03-252285 be changed by increasing the maximum production of the batch digester system from 87.3 TPH ADUP to 120 TPH and including a maximum daily pulp production rate of 2,096.3 TPD ADUP. KBN noted that these changes were consistent with the original permit which identified a pulp production capacity of 120 TPH, and that the monthly averaged, daily limit would insure no increase in air emissions. As such Stone requests that language in SC 15 of the construction permit, and SC 2 of the operation permit be changed as follows:

FROM:

AC03-252285:

SC 5: The maximum production rate will be 87.3 tons per hour air dried unbleached pulp (ADUP).

AO03-270940:

SC 2: The maximum allowable operating rate is 87.3 tons per hour air dried unbleached pulp (ADUP) per hour.

TO:

The maximum allowable operating rate is 120 tons per hour air dried unbleached pulp (ADUP), and 2096.3 tons per day ADUP (monthly average).

Permit AC03-142979 was issued September 24, 1989 by DARM and identified a maximum production rate of 120 tons ADUP per hour and 1911 tons of ADUP per day. This permit identified the maximum production rate for testing purposes to 79.6 tons of ADUP per hour. Subsequently permit AO03-174790 was issued August 10, 1990; and, specific condition 15 limited the maximum production of the digester systems to 120 tons ADUP per hour, but for testing purposes limited production of the digester system to 79.6 tons ADUP per hour.

Construction permit AC03-252285 was issued July 5, 1994 allowing replacement of the 22 digester systems; and, included a condition limiting the maximum production rate to 87.3 tons per hour ADUP. The application (see page ATT-2) identifies maximum

Stone Container Corporation
North American Containerboard,
Paper and Pulp Division

Panama City Mill

Post Office Box 2560
Panama City, Florida 32402

(904) 785-4311

May 10, 1995

Mr. Ed Middleswart, P.E.
Air Resource Management
Department of Environmental Protection
160 Governmental Center
Pensacola, Florida 32501-5794

Dear Mr. Middleswart:

Enclosed are four (4) copies of an operating permit application for the digester system at the Panama City Mill of Stone Container Corporation. Also enclosed is a TRS venting contingency plan.

If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Yours truly,

L.D. Riley, Jr.
Environmental Superintendent

LDR/mw
cc: J. Prescott/C. Bogatie (w/o encl.)
David Buff - KBN Engineering

Emissions Unit Information Section 1 of 1

Emissions Unit Control Equipment

1. Description: Incineration of TRS gases in the lime kiln (No. 4 Bark Boiler is backup)
2. Control Device or Method Code(s): 022

Emissions Unit Operating Capacity

1. Maximum Heat Input Rate:	mmBtu/hr	
2. Maximum Incineration Rate:	lb/hr	tons/day
3. Maximum Process or Throughput Rate:		
4. Maximum Production Rate: 87.3 TPH air dried unbleached pulp		
5. Operating Capacity Comment:		

Emissions Unit Operating Schedule

Requested Maximum Operating Schedule:			
	24 hours/day	7 days/week	
	52 weeks/year	8,760 hours/year	

permit AC03-174790; limit 120 tons (ADUB)/hr
test purposes - 79.6

CP goal - 78.6 ADUB/hr

Stone Container Corporation

Containerboard and Paper Division

Panama City Mill

Post Office Box 2560
Panama City, Florida 32402

(904) 785 4311

May 16, 1994

Mr. Ed Middleswart, P.E.
Air Resources Management
Department of Environmental Protection
160 Governmental Center
Pensacola, FL 32501-5794

Dear Mr. Middleswart:

On April 13, we had a catastrophic failure of a batch digester at the Panama City Mill of Stone Container Corporation. Because of the extensive damage caused by the failure and the age of the remaining undamaged digesters (16 of 22), it has been determined that the most prudent course of action is to replace all the digesters at this time.

The digesters will be replaced in kind; therefore, there will be no production increase because of this project. Noncondensable gasses from the new digesters and the turpentine recovery system will be collected in the existing NCG collection and incineration system just as the gasses from the old digester system were. The NCG collecting system was not damaged by the failure; therefore, repairs and alterations to this system are not necessary.

It is our opinion that this project does not require permitting for the following reasons:

1. The digesters are being replace in kind and in the identical location or the old digesters.

2. There will be no production increase resulting from this project.

3. The existing air emissions control system will be used for the new digesters.

4. There will be no increase in air or water pollutants.

Please confirm your concurrence with this opinion to us in writing.

Stone Container Corporation

Containerboard and Paper Division

Panama City Mill

Post Office Box 2560
Panama City, Florida 32402

(904) 785-4311

June 3, 1994

Mr. Ed Middleswart, P.E.
Air Resource Management
Department of Environmental Regulation
160 Governmental Center
Pensacola, Florida 32501-5794

Dear Mr. Middleswart:

Enclosed are four copies of the construction permit applications to install the replacement digesters at the Panama City Mill of Stone Container Corporation. Please note that these digesters are identical replacements for the digesters being removed from service because of the catastrophic failure we experienced in April, 1994. Also note that the existing NCG system will be used for TRS control, since it was not damaged by the explosion.

If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Sincerely yours,

L.D. Riley, Jr.
Environmental Superintendent

RECEIVED
JUN - 6 1994
Northwest Florida
DEP

/mkd

cc: Jack B. Prescott

If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Yours truly,

L. D. Riley, Jr.

L. D. Riley, Jr.
Environmental Superintendent

/mkd

CC: Jack Prescott

ATTACHMENT A

1.0 PROCESS DESCRIPTION

Stone Container Corporation (SCC) owns and operates a kraft pulp mill located in Panama City, Florida. The facility includes twenty-two (22) batch digesters which are used to cook wood chips to produce pulp for the paper and linerboard making process. The location of the mill in relation to the surrounding area is shown in Figure 1. A plot plan of the mill is presented in Figure 2.

Recently, a catastrophic accident took place at the mill involving the batch digester system. One of the digester structures failed, resulting in severe damage to the digester as well as several other digesters. After careful study, SCC has decided to replace all of the batch digesters at the mill, in order to reduce the potential for further digester structure failures.

The existing batch digester system is permitted under Florida Department of Environmental Protection (FDEP) operating permit AC03-174790 issued on August 10, 1990. The maximum permitted production rate of the system is 120 tons per hour (TPH) of air dried unbleached pulp (ADUP).

A flow diagram of the digester system which is now in operation at SCC is shown in Figure 3. The arrangement of the 22 batch digesters and blow tanks is shown in Figure 4.

As shown in Figures 3 and 4, the batch digester system at SCC consists of 22 batch digesters, five (5) blow tanks, and one (1) accumulator tank. Condensers are located before and after the accumulator tank in order to collect condensibles from the gas/vapor stream. A turpentine condensing system also follows the accumulator in order to recover turpentine from the system.

Although each of the 22 batch digesters is essentially identical, eight (8) are designated to produce primary pulp, twelve (12) are designated to produce easy bleached kraft (EBK) pulp, and two (2) are designated to produce secondary pulp. The system is arranged such that the two secondary pulp digesters discharge to the No. 1 Blow Tank. Three of the primary digesters can discharge to either the No. 1 Blow Tank or the No. 2 Blow Tank. Two other primary digesters discharge only to the No. 2 Blow Tank. The remaining three primary digesters discharge to the No. 4 Blow Tank.

Of the twelve EBK digesters, one can discharge to either the No. 3 or No. 4 Blow Tank, five discharge only to the No. 3 Blow tank, and six discharge only to the No. 5 Blow Tank.

As shown in Figure 3, non-condensible gases (NCG) from the batch digesters, blow tanks, accumulator tank and turpentine condenser system are collected and sent to the Lime Kiln at the facility for destruction of total reduced sulfur (TRS). The No. 4 Bark Boiler is used as a backup destruction device.

SCC is proposing to replace all twenty two of the existing batch digesters. However, the remainder of the batch digester system, including the NCG incineration system, will not be replaced or modified. Each of the new digesters will be approximately 2,600 cubic feet in size. The maximum process rate of the digester system will not increase as a result of these changes.

2.0 DERIVATION OF PROCESS INPUT RATES

The future maximum input of raw materials to the digesters and the maximum product weights are based upon the following:

Maximum 24-hour pulp production:

= 1,886.7 TPD, dry basis

= 157,225 lb/hr, dry basis, 24-hour maximum. ≈ 78.6 TPH pulp

EBK Pulp (12 digesters)

Raw material inputs per digester per blow:

31.25 tons wood chips = 62,500 lbs

6,500 gal white liquor @ 9.9 lb/gal = 64,350 lbs

3,000 gal weak black liquor @ 8.6 lb/gal = 25,800 lbs

Total input per blow = 62,500 + 64,350 + 25,800 = 152,650 lbs

Maximum blows per day = 120 total for 12 digesters

Blows per hour = 5

Total raw material input:

Wood chips = 62,500 lbs/blow x 5 blows/hr = 312,500 lbs/hr

White liquor = 64,350 lbs/blow x 5 blows/hr = 321,750 lbs/hr

Weak black liquor = 25,800 lbs/blow x 5 blows/day = 129,000 lbs/hr

Total = 312,500 + 321,750 + 129,000 = 763,250 lbs/hr

Primary Pulp (8 digesters)

Raw material inputs per digester per blow:

31.25 tons wood chips = 62,500 lbs

3,500 gal white liquor @ 9.9 lb/gal = 34,650 lbs

5,000 gal weak black liquor @ 8.6 lb/gal = 43,000 lbs

Total input per blow = 62,500 + 34,650 + 43,000 = 140,150 lbs

Maximum blows per day = 95 total for 8 digesters

Blows per hour = 4

Total raw material input:

Wood chips = 62,500 lbs/blow x 4 blows/hr = 250,000 lbs/hr

White liquor = 34,650 lbs/blow x 4 blows/hr = 138,600 lbs/hr

Weak black liquor = 43,000 lbs/blow x 4 blows/day = 172,000 lbs/hr

Total = 250,000 + 138,600 + 172,000 = 560,600 lbs/hr

Secondary Pulp (2 digesters)

Raw material inputs per digester per blow:

31.25 tons wood chips = 62,500 lbs

5,000 gal white liquor @ 9.9 lb/gal = 49,500 lbs

3,500 gal weak black liquor @ 8.6 lb/gal = 30,100 lbs

Total input per blow = 62,500 + 49,500 + 30,100 = 142,100 lbs

Maximum blows per day = 16 total for 2 digesters

Blows per hour = 0.67

Total raw material input:

Wood chips = 62,500 lbs/blow x 0.67 blows/hr = 41,875 lbs/hr

White liquor = 49,500 lbs/blow x 0.67 blows/hr = 33,165 lbs/hr

Weak black liquor = 30,100 lbs/blow x 0.67 blows/day = 20,167 lbs/hr

Total = 41,875 + 33,165 + 20,167 = 95,207 lbs/hr

Total Process Input Rate For All Digesters

Total process input rate = EBK + Primary + Secondary pulp

Total wood chips: 312,500 + 250,000 + 41,875 = 604,375 lbs/hr

Total white liquor = 321,750 + 138,600 + 33,165 = 493,515 lbs/hr

Total weak black liquor = 129,000 + 172,000 + 20,167 = 321,167 lbs/hr

Total = 604,375 + 493,515 + 321,167 = 1,418,709 lb/hr

3.0 TRS EMISSION ESTIMATES

TRS emission estimates are based upon TRS emission factors published in EPA Publication AP-42. The emission factor is based on tons of air dried unbleached pulp (ADUP), which contains approximately 10 percent moisture.

1,886.7 TPD dry pulp ÷ (1 - 0.1) = 2,096.3 TPD ADUP

TRS emissions = 2,096.3 TPD ADUP x 1.2 lb/ton ADUP ÷ 24 hr/day

= 104.8 lb/hr TRS

2,096.3 TPD ADUP x 1.2 lb/ton x 365 days/yr ÷ 2,000 lb/ton = 459.1 TPY

The TRS emissions from the digester system are controlled by venting the gases to the lime kiln or the No. 4 Bark Boiler for incineration. The TRS gases will be subject to a temperature of at least 1,200°F for at least 0.5 seconds in either of these combustion devices.

Post-it® Fax Note 7671	Date 4/30/02 # of pages ▶ 10
To BRUCE MITCHELL	From RICK BRADBURN
Co./Dept. DARM	Co. NWD AIR
Phone #	Phone # SC 695 8364
Fax # SC 292-6979	Fax # x1233

To: Andy Allen
From: Bob Kriegel
Date: June 6, 1996

Re: **Letter Request from Stone Container, Bay County to change Permitted Production Rates; EMU ID no. 0050009027, permit no. AO03-270940**

By letter dated May 24, 1996 KBN requested that Stone Container Corporation permits AO03-270940 and AC03-252285 be changed by increasing the maximum production of the batch digester system from 87.3 TPH ADUP to 120 TPH and including a maximum daily pulp production rate of 2,096.3 TPD ADUP. KBN noted that these changes were consistent with the original permit which identified a pulp production capacity of 120 TPH, and that the monthly averaged, daily limit would insure no increase in air emissions. As such Stone requests that language in SC 15 of the construction permit, and SC 2 of the operation permit be changed as follows:

FROM:

AC03-252285:

SC 5: The maximum production rate will be 87.3 tons per hour air dried unbleached pulp (ADUP).

AO03-270940:

SC 2: The maximum allowable operating rate is 87.3 tons per hour air dried unbleached pulp (ADUP) per hour.

TO:

The maximum allowable operating rate is 120 tons per hour air dried unbleached pulp (ADUP), and 2096.3 tons per day ADUP (monthly average).

Permit AC03-142979 was issued September 24, 1989 by DARM and identified a maximum production rate of 120 tons ADUP per hour and 1911 tons of ADUP per day. This permit identified the maximum production rate for testing purposes to 79.6 tons of ADUP per hour. Subsequently permit AO03-174790 was issued August 10, 1990; and, specific condition 15 limited the maximum production of the digester systems to 120 tons ADUP per hour, but for testing purposes limited production of the digester system to 79.6 tons ADUP per hour.

Construction permit AC03-252285 was issued July 5, 1994 allowing replacement of the 22 digester systems; and, included a condition limiting the maximum production rate to 87.3 tons per hour ADUP. The application (see page ATT-2) identifies maximum

Stone Container Corporation
North American Containerboard,
Paper and Pulp Division

Panama City Mill

Post Office Box 2560
Panama City, Florida 32402

(904) 785-4311

May 10, 1995

Mr. Ed Middleswart, P.E.
Air Resource Management
Department of Environmental Protection
160 Governmental Center
Pensacola, Florida 32501-5794

Dear Mr. Middleswart:

Enclosed are four (4) copies of an operating permit application for the digester system at the Panama City Mill of Stone Container Corporation. Also enclosed is a TRS venting contingency plan.

If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Yours truly,

L.D. Riley, Jr.
Environmental Superintendent

LDR/mw
cc: J. Prescott/C. Bogatie (w/o encl.)
David Buff - KBN Engineering

Emissions Unit Information Section 1 of 1

Emissions Unit Control Equipment

1. Description: Incineration of TRS gases in the lime kiln (No. 4 Bark Boiler is backup)
2. Control Device or Method Code(s): 022

Emissions Unit Operating Capacity

1. Maximum Heat Input Rate:	mmBtu/hr	
2. Maximum Incineration Rate:	lb/hr	tons/day
3. Maximum Process or Throughput Rate:		
4. Maximum Production Rate: 87.3 TPH air dried unbleached pulp		
5. Operating Capacity Comment:		

Emissions Unit Operating Schedule

Requested Maximum Operating Schedule:			
	24 hours/day	7 days/week	
	52 weeks/year	8,760 hours/year	

permit 0003-174790; limit 120 tons(ADUB)/hr
test purposes - 79.6

CP application - 78.6 ADUB/hr

Stone Container Corporation

Containerboard and Paper Division

Panama City Mill

Post Office Box 2560
Panama City, Florida 32402

(904) 785 4311

May 16, 1994

Mr. Ed Middleswart, P.E.
Air Resources Management
Department of Environmental Protection
160 Governmental Center
Pensacola, FL 32501-5794

Dear Mr. Middleswart:

On April 13, we had a catastrophic failure of a batch digester at the Panama City Mill of Stone Container Corporation. Because of the extensive damage caused by the failure and the age of the remaining undamaged digesters (16 of 22), it has been determined that the most prudent course of action is to replace all the digesters at this time.

The digesters will be replaced in kind; therefore, there will be no production increase because of this project. Noncondensable gasses from the new digesters and the turpentine recovery system will be collected in the existing NCG collection and incineration system just as the gasses from the old digester system were. The NCG collecting system was not damaged by the failure; therefore, repairs and alterations to this system are not necessary.

It is our opinion that this project does not require permitting for the following reasons:

1. The digesters are being replace in kind and in the identical location of the old digesters.

2. There will be no production increase resulting from this project.

3. The existing air emissions control system will be used for the new digesters.

4. There will be no increase in air or water pollutants.

Please confirm your concurrence with this opinion to us in writing.

Stone Container Corporation

Containerboard and Paper Division

Panama City Mill

Post Office Box 2560
Panama City, Florida 32402

(904) 785-4311

June 3, 1994

Mr. Ed Middleswart, P.E.
Air Resource Management
Department of Environmental Regulation
160 Governmental Center
Pensacola, Florida 32501-5794

Dear Mr. Middleswart:

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If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Sincerely yours,

L.D. Riley, Jr.
Environmental Superintendent

RECEIVED
JUN - 6 1994
Northwest Florida
DEP

/mkd

cc: Jack B. Prescott

If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Yours truly,

L. D. Riley, Jr.

L. D. Riley, Jr.
Environmental Superintendent

/mkd

CC: Jack Prescott

ATTACHMENT A

1.0 PROCESS DESCRIPTION

Stone Container Corporation (SCC) owns and operates a kraft pulp mill located in Panama City, Florida. The facility includes twenty-two (22) batch digesters which are used to cook wood chips to produce pulp for the paper and linerboard making process. The location of the mill in relation to the surrounding area is shown in Figure 1. A plot plan of the mill is presented in Figure 2.

Recently, a catastrophic accident took place at the mill involving the batch digester system. One of the digester structures failed, resulting in severe damage to the digester as well as several other digesters. After careful study, SCC has decided to replace all of the batch digesters at the mill, in order to reduce the potential for further digester structure failures.

The existing batch digester system is permitted under Florida Department of Environmental Protection (FDEP) operating permit AC03-174790 issued on August 10, 1990. The maximum permitted production rate of the system is 120 tons per hour (TPH) of air dried unbleached pulp (ADUP).

A flow diagram of the digester system which is now in operation at SCC is shown in Figure 3. The arrangement of the 22 batch digesters and blow tanks is shown in Figure 4.

As shown in Figures 3 and 4, the batch digester system at SCC consists of 22 batch digesters, five (5) blow tanks, and one (1) accumulator tank. Condensers are located before and after the accumulator tank in order to collect condensibles from the gas/vapor stream. A turpentine condensing system also follows the accumulator in order to recover turpentine from the system.

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Of the twelve EBK digesters, one can discharge to either the No. 3 or No. 4 Blow Tank, five discharge only to the No. 3 Blow tank, and six discharge only to the No. 5 Blow Tank.

As shown in Figure 3, non-condensible gases (NCG) from the batch digesters, blow tanks, accumulator tank and turpentine condenser system are collected and sent to the Lime Kiln at the facility for destruction of total reduced sulfur (TRS). The No. 4 Bark Boiler is used as a backup destruction device.

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2.0 DERIVATION OF PROCESS INPUT RATES

The future maximum input of raw materials to the digesters and the maximum product weights are based upon the following:

Maximum 24-hour pulp production:

= 1,886.7 TPD, dry basis

= 157,225 lb/hr, dry basis, 24-hour maximum. ≈ 78.6 TPH pulp

EBK Pulp (12 digesters)

Raw material inputs per digester per blow:

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6,500 gal white liquor @ 9.9 lb/gal = 64,350 lbs

3,000 gal weak black liquor @ 8.6 lb/gal = 25,800 lbs

Total input per blow = 62,500 + 64,350 + 25,800 = 152,650 lbs

Maximum blows per day = 120 total for 12 digesters

Blows per hour = 5

Total raw material input:

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White liquor = 64,350 lbs/blow x 5 blows/hr = 321,750 lbs/hr

Weak black liquor = 25,800 lbs/blow x 5 blows/day = 129,000 lbs/hr

Total = 312,500 + 321,750 + 129,000 = 763,250 lbs/hr

Primary Pulp (8 digesters)

Raw material inputs per digester per blow:

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Maximum blows per day = 95 total for 8 digesters

Blows per hour = 4

Total raw material input:

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Total = 41,875 + 33,165 + 20,167 = 95,207 lbs/hr

Total Process Input Rate For All Digesters

Total process input rate = EBK + Primary + Secondary pulp

Total wood chips: 312,500 + 250,000 + 41,875 = 604,375 lbs/hr

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Total = 604,375 + 493,515 + 321,167 = 1,418,709 lb/hr

3.0 TRS EMISSION ESTIMATES

TRS emission estimates are based upon TRS emission factors published in EPA Publication AP-42. The emission factor is based on tons of air dried unbleached pulp (ADUP), which contains approximately 10 percent moisture.

1,886.7 TPD dry pulp ÷ (1 - 0.1) = 2,096.3 TPD ADUP

TRS emissions = 2,096.3 TPD ADUP x 1.2 lb/ton ADUP ÷ 24 hr/day

= 104.8 lb/hr TRS

2,096.3 TPD ADUP x 1.2 lb/ton x 365 days/yr ÷ 2,000 lb/ton = 459.1 TPY

The TRS emissions from the digester system are controlled by venting the gases to the lime kiln or the No. 4 Bark Boiler for incineration. The TRS gases will be subject to a temperature of at least 1,200°F for at least 0.5 seconds in either of these combustion devices.

Stone Container Corporation

Containerboard and Paper Division

Panama City Mill

Post Office Box 2560
Panama City, Florida 32402

(904) 785 4311

May 16, 1994

Mr. Ed Middleswart, P.E.
Air Resources Management
Department of Environmental Protection
160 Governmental Center
Pensacola, FL 32501-5794

Dear Mr. Middleswart:

On April 13, we had a catastrophic failure of a batch digester at the Panama City Mill of Stone Container Corporation. Because of the extensive damage caused by the failure and the age of the remaining undamaged digesters (16 of 22), it has been determined that the most prudent course of action is to replace all the digesters at this time.

The digesters will be replaced in kind; therefore, there will be no production increase because of this project. Noncondensable gasses from the new digesters and the turpentine recovery system will be collected in the existing NCG collection and incineration system just as the gasses from the old digester system were. The NCG collecting system was not damaged by the failure; therefore, repairs and alterations to this system are not necessary.

It is our opinion that this project does not require permitting for the following reasons:

1. The digesters are being replace in kind and in the identical location of the old digesters.

2. There will be no production increase resulting from this project.

3. The existing air emissions control system will be used for the new digesters.

4. There will be no increase in air or water pollutants.

Please confirm your concurrence with this opinion to us in writing.

Stone Container Corporation

Containerboard and Paper Division

Panama City Mill

Post Office Box 2560
Panama City, Florida 32402

(904) 785-4311

June 3, 1994

Gdm
6/6

Mr. Ed Middleswart, P.E.
Air Resource Management
Department of Environmental Regulation
160 Governmental Center
Pensacola, Florida 32501-5794

Dear Mr. Middleswart:

Enclosed are four copies of the construction permit applications to install the replacement digesters at the Panama City Mill of Stone Container Corporation. Please note that these digesters are identical replacements for the digesters being removed from service because of the catastrophic failure we experienced in April, 1994. Also note that the existing NCG system will be used for TRS control, since it was not damaged by the explosion.

If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Sincerely yours,

L.D. Riley, Jr.
Environmental Superintendent

RECEIVED
JUN - 6 1994
Northwest Florida
DEP

/mkd

cc: Jack B. Prescott

If you have any questions or comments, please contact David Riley at (904) 785-4311, Ext. 257.

Yours truly,

L. D. Riley, Jr.

L. D. Riley, Jr.
Environmental Superintendent

/mkd

CC: Jack Prescott

ATTACHMENT A

1.0 PROCESS DESCRIPTION

Stone Container Corporation (SCC) owns and operates a kraft pulp mill located in Panama City, Florida. The facility includes twenty-two (22) batch digesters which are used to cook wood chips to produce pulp for the paper and linerboard making process. The location of the mill in relation to the surrounding area is shown in Figure 1. A plot plan of the mill is presented in Figure 2.

Recently, a catastrophic accident took place at the mill involving the batch digester system. One of the digester structures failed, resulting in severe damage to the digester as well as several other digesters. After careful study, SCC has decided to replace all of the batch digesters at the mill, in order to reduce the potential for further digester structure failures.

The existing batch digester system is permitted under Florida Department of Environmental Protection (FDEP) operating permit AO03-174790 issued on August 10, 1990. The maximum permitted production rate of the system is 120 tons per hour (TPH) of air dried unbleached pulp (ADUP).

A flow diagram of the digester system which is now in operation at SCC is shown in Figure 3. The arrangement of the 22 batch digesters and blow tanks is shown in Figure 4.

As shown in Figures 3 and 4, the batch digester system at SCC consists of 22 batch digesters, five (5) blow tanks, and one (1) accumulator tank. Condensers are located before and after the accumulator tank in order to collect condensibles from the gas/vapor stream. A turpentine condensing system also follows the accumulator in order to recover turpentine from the system.

Although each of the 22 batch digesters is essentially identical, eight (8) are designated to produce primary pulp, twelve (12) are designated to produce easy bleached kraft (EBK) pulp, and two (2) are designated to produce secondary pulp. The system is arranged such that the two secondary pulp digesters discharge to the No. 1 Blow Tank. Three of the primary digesters can discharge to either the No. 1 Blow Tank or the No. 2 Blow Tank. Two other primary digesters discharge only to the No. 2 Blow Tank. The remaining three primary digesters discharge to the No. 4 Blow Tank.

Of the twelve EBK digesters, one can discharge to either the No. 3 or No. 4 Blow Tank, five discharge only to the No. 3 Blow tank, and six discharge only to the No. 5 Blow Tank.

As shown in Figure 3, non-condensible gases (NCG) from the batch digesters, blow tanks, accumulator tank and turpentine condenser system are collected and sent to the Lime Kiln at the facility for destruction of total reduced sulfur (TRS). The No. 4 Bark Boiler is used as a backup destruction device.

SCC is proposing to replace all twenty two of the existing batch digesters. However, the remainder of the batch digester system, including the NCG incineration system, will not be replaced or modified. Each of the new digesters will be approximately 2,600 cubic feet in size. The maximum process rate of the digester system will not increase as a result of these changes.

2.0 DERIVATION OF PROCESS INPUT RATES

The future maximum input of raw materials to the digesters and the maximum product weights are based upon the following:

Maximum 24-hour pulp production:

= 1,886.7 TPD, dry basis

= 157,225 lb/hr, dry basis, 24-hour maximum. = 78.6 TPH pulp.

EBK Pulp (12 digesters)

Raw material inputs per digester per blow:

31.25 tons wood chips = 62,500 lbs

6,500 gal white liquor @ 9.9 lb/gal = 64,350 lbs

3,000 gal weak black liquor @ 8.6 lb/gal = 25,800 lbs

Total input per blow = 62,500 + 64,350 + 25,800 = 152,650 lbs

Maximum blows per day = 120 total for 12 digesters

Blows per hour = 5

Total raw material input:

Wood chips = 62,500 lbs/blow x 5 blows/hr = 312,500 lbs/hr

White liquor = 64,350 lbs/blow x 5 blows/hr = 321,750 lbs/hr

Weak black liquor = 25,800 lbs/blow x 5 blows/day = 129,000 lbs/hr

Total = 312,500 + 321,750 + 129,000 = 763,250 lbs/hr

Primary Pulp (8 digesters)

Raw material inputs per digester per blow:

31.25 tons wood chips = 62,500 lbs

3,500 gal white liquor @ 9.9 lb/gal = 34,650 lbs

5,000 gal weak black liquor @ 8.6 lb/gal = 43,000 lbs

Total input per blow = 62,500 + 34,650 + 43,000 = 140,150 lbs

Maximum blows per day = 95 total for 8 digesters

Blows per hour = 4

Total raw material input:

Wood chips = 62,500 lbs/blow x 4 blows/hr = 250,000 lbs/hr

White liquor = 34,650 lbs/blow x 4 blows/hr = 138,600 lbs/hr

Weak black liquor = 43,000 lbs/blow x 4 blows/day = 172,000 lbs/hr

Total = 250,000 + 138,600 + 172,000 = 560,600 lbs/hr

Secondary Pulp (2 digesters)

Raw material inputs per digester per blow:

31.25 tons wood chips = 62,500 lbs

5,000 gal white liquor @ 9.9 lb/gal = 49,500 lbs

3,500 gal weak black liquor @ 8.6 lb/gal = 30,100 lbs

Total input per blow = 62,500 + 49,500 + 30,100 = 142,100 lbs

Maximum blows per day = 16 total for 2 digesters

Blows per hour = 0.67

Total raw material input:

Wood chips = 62,500 lbs/blow x 0.67 blows/hr = 41,875 lbs/hr

White liquor = 49,500 lbs/blow x 0.67 blows/hr = 33,165 lbs/hr

Weak black liquor= 30,100 lbs/blow x 0.67 blows/day = 20,167 lbs/hr

Total = 41,875 + 33,165 + 20,167 = 95,207 lbs/hr

Total Process Input Rate For All Digesters

Total process input rate = EBK + Primary + Secondary pulp

Total wood chips: 312,500 + 250,000 + 41,875 = 604,375 lbs/hr

Total white liquor = 321,750 + 138,600 + 33,165 = 493,515 lbs/hr

Total weak black liquor = 129,000 + 172,000 + 20,167 = 321,167 lbs/hr

Total = 604,375 + 493,515 + 321,167 = 1,418,709 lb/hr

3.0 TRS EMISSION ESTIMATES

TRS emission estimates are based upon TRS emission factors published in EPA Publication AP-42. The emission factor is based on tons of air dried unbleached pulp (ADUP), which contains approximately 10 percent moisture.

1,886.7 TPD dry pulp ÷ (1 - 0.1) = 2,096.3 TPD ADUP

TRS emissions = 2,096.3 TPD ADUP x 1.2 lb/ton ADUP ÷ 24 hr/day

= 104.8 lb/hr TRS

2,096.3 TPD ADUP x 1.2 lb/ton x 365 days/yr ÷ 2,000 lb/ton = 459.1 TPY

The TRS emissions from the digester system are controlled by venting the gases to the lime kiln or the No. 4 Bark Boiler for incineration. The TRS gases will be subject to a temperature of at least 1,200°F for at least 0.5 seconds in either of these combustion devices.

Department of Environmental Protection

Lawton Chiles
Governor

Northwest District
160 Governmental Center
Pensacola, Florida 32501-5794

Virginia B. Wetherell
Secretary

PERMITTEE:

Stone Container Corporation

I.D. Number: 10PCY03000927
Permit/Certification Number: AC03-252285
Date of Issue: July 5, 1994
Expiration Date: June 15, 1995
County: Bay
Latitude/Longitude:30°08'30"N/85°37'25"W
Project: Digester System Rebuild

This permit is issued under the provisions of section 403.087,Florida Statutes, and Florida Administrative Code Rules 17-296, 17-297 and 17-4. The above named applicant, hereinafter called permittee, is hereby authorized to perform the work or operate the facility shown on the application and approved drawings, plans, and other documents attached hereto or on file with the Department and made a part hereof and specifically described as follows:

The 22 digester systems will be replaced in kind and the emissions will be totally contained in the existing NCG collection system and routed to the lime kiln for incineration. The No. 4 Bark Boiler serves as backup to the lime kiln for TRS incineration. The TRS gases will be subjected to a minimum temperature of 1200 degrees Fahrenheit for at least 0.5 seconds in either of the two combustion devices. The 22 batch digester systems consist of five blow tanks, one accumulator tank with a condenser before and after the accumulator tank and a turpentine condensing system following the accumulator. The maximum process rate will not increase as a result of the new digester system.

The project is located at the permittee's kraft pulp mill in Panama City, Bay County, Florida. The UTM coordinates are zone 16, 632.8 km East, and 3335.1 km North.

The Standard Industrial Codes are:
Industry No. 2611-Pulp Mills
~~Industry No. 2621-Paper Mills~~ ℓ.m.

The Standard Classification Codes are:
Pulp and Paper Industry Major Group 26:
Sulfate (Kraft) Pulping
BATCH DIGESTER SYSTEM 3-07-001-01
TERPENE CONDENSER 3-07-001-07

PERMITTEE:

Stone Container Corporation

I.D. Number: 10PCY03000927
Permit/Certification Number: AC03-252285
Date of Issue: July 5, 1994
Expiration Date: June 15, 1995

SPECIFIC CONDITIONS:

General

1. The attached General Conditions are part of this permit. [FAC Rule 17-4.160]

Construction

2. The Department shall be notified upon initial commissioning of the new Digester system. [FAC Rule 17-4.210]

3. The Department shall be notified and prior approval obtained of any changes or revisions from the June 6, 1994 application. [FAC Rule 17-4.210]

Operation

4. The digester system may operate continuously (8760 hours per year). [FAC Rule 17-4.070]

5. The maximum production rate will be 87.3 tons per hour air dried unbleached pulp (ADUP). [FAC Rule 17-4.070]

6. The non-condensible gases (NCG) from the batch digesters, blow tanks, accumulator tank and turpentine condenser system shall be destroyed in the Lime Kiln or the Bark Boiler by subjecting the TRS gases to at least 1200°F for at least 0.5 seconds. [FAC Rule 17-296.404(3)(e)]

7. The digester system is subject to the total reduced sulfur (TRS) emission limiting standard which requires combustion of the TRS gases in the lime kiln. [FAC Rule 17-296.404(3)(a)1]

Administrative

8. Submit an updated TRS VENTING CONTINGENCY PLAN with the request for the operation permit. The plan shall include definitions of what constitutes a reportable venting incident and an assessment of the use of the back-up control device.[17-296.404(3)3]

9. The new process equipment shall be installed in such a manner to facilitate regular inspections and maintenance to minimize fugitive gaseous emissions. [FAC Rule 17-4.070]

10. An annual operation report shall be submitted by March 1 each year. [FAC Rule 17-210.370]

11. A major air pollution source Annual Operation Fee Form must be completed and submitted with the appropriate fee between January 15 and March 1 of each year.[FAC Rule 17-213]

Department of Environmental Protection

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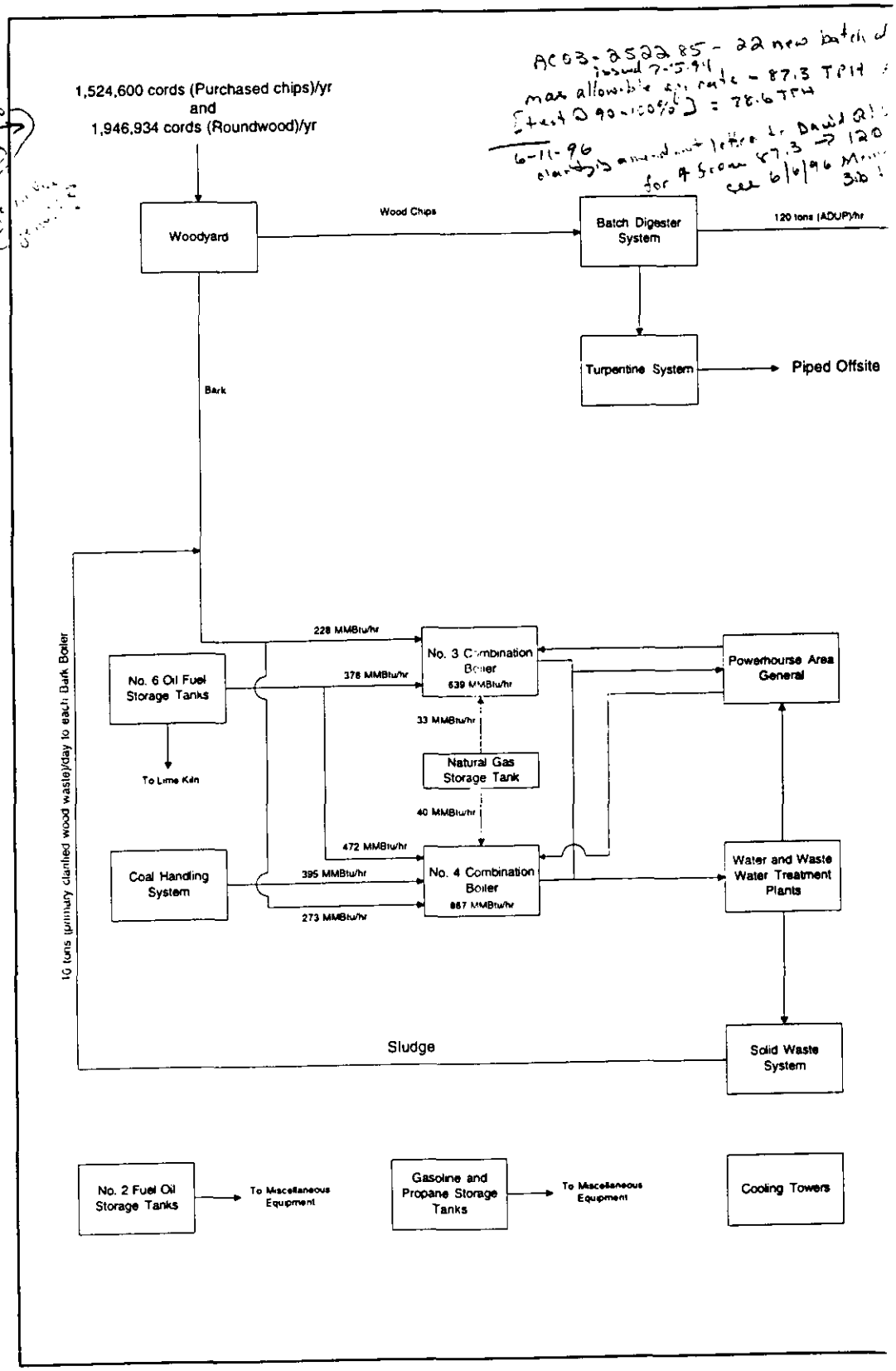

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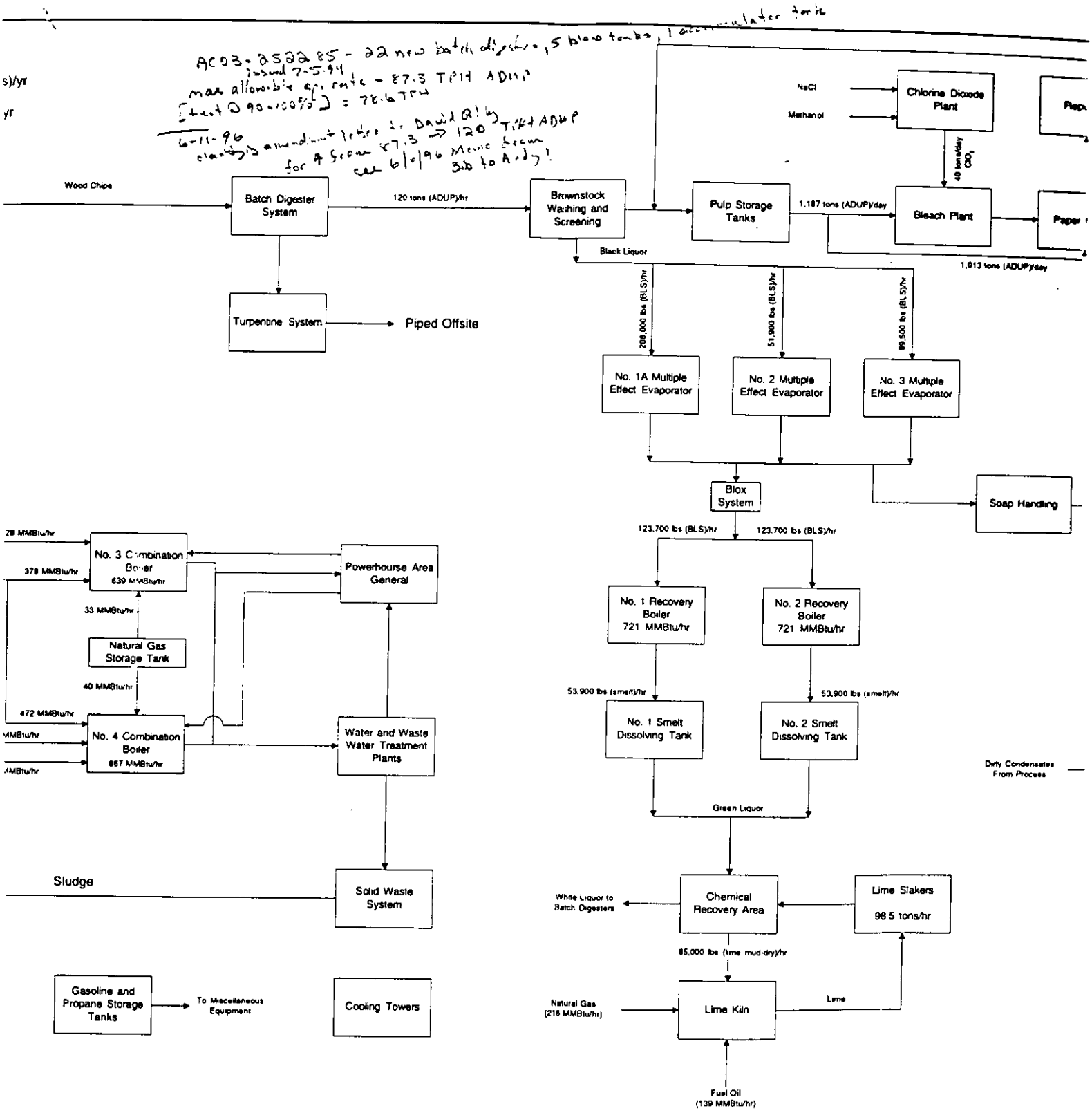

AC03-252285 - 22 new batch digesters, 5 blow tanks, 1 accumulator tank
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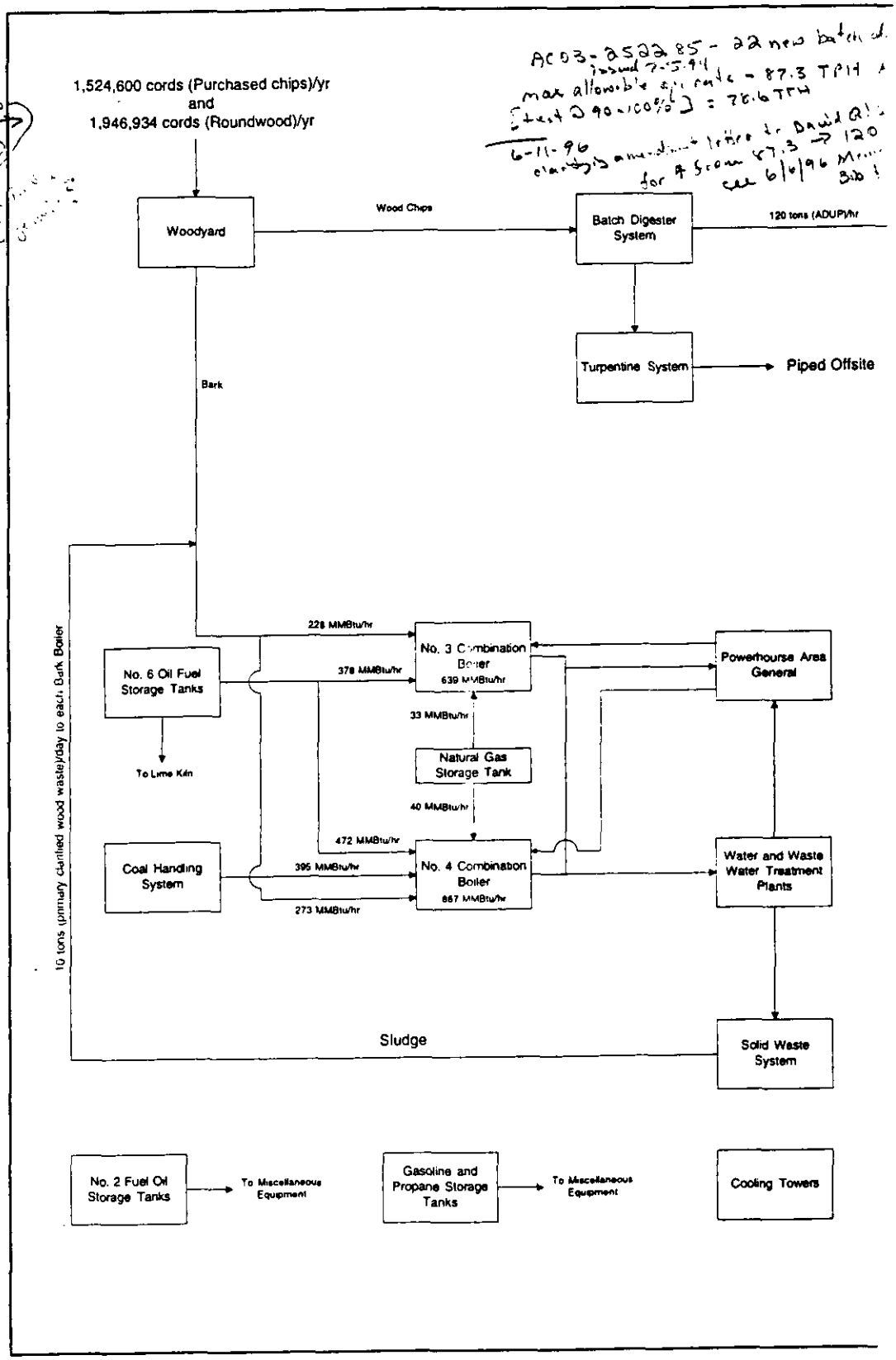
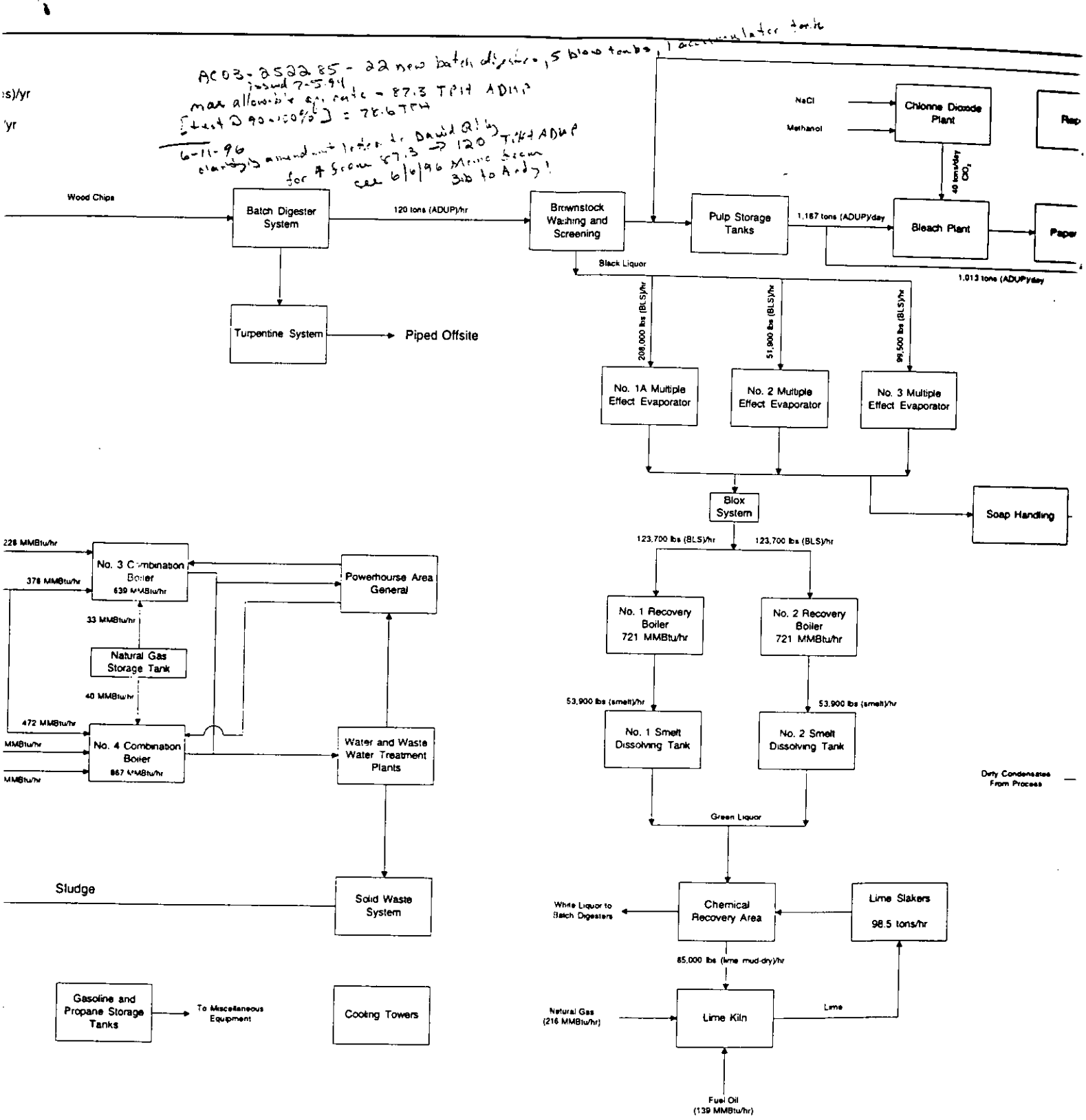
max allowable operate - 87.3 TPH ADUP
[test @ 90-100%] = 78.6 TPH
6-11-96 clarify amendment letter to David Gilg 120 TPH ADUP
for A Screen 87.3 ⇒ 120 Memo from
see 6/6/96 310 to Addy!

Corporation	Emission Unit: Facility	
	Process Area: Overall Plant Flow Diagram	
Panama City, FL	Filename: 9937518Y/F1/WP/SCC-FAC.VSD	
	Latest Revision Date: 4/5/00 4:01 PM	



Stone Container Corporation	
SCC-FI-C3	Panama City, FL

Emission Unit: Facility
Process Area: Overall Plant Flow Diag
Filename: 9937518Y/F1/WP/SCC
Latest Revision Date:



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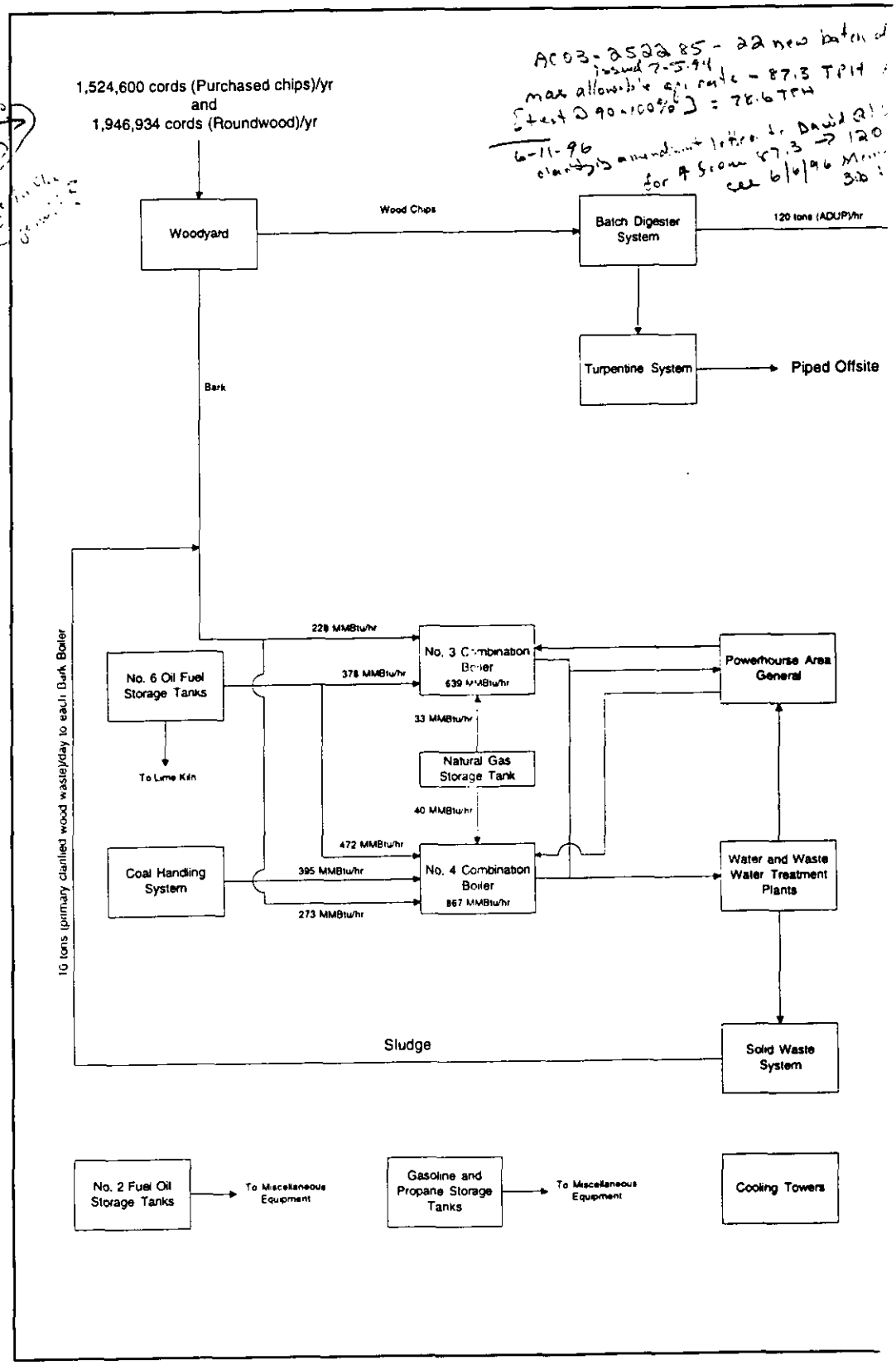

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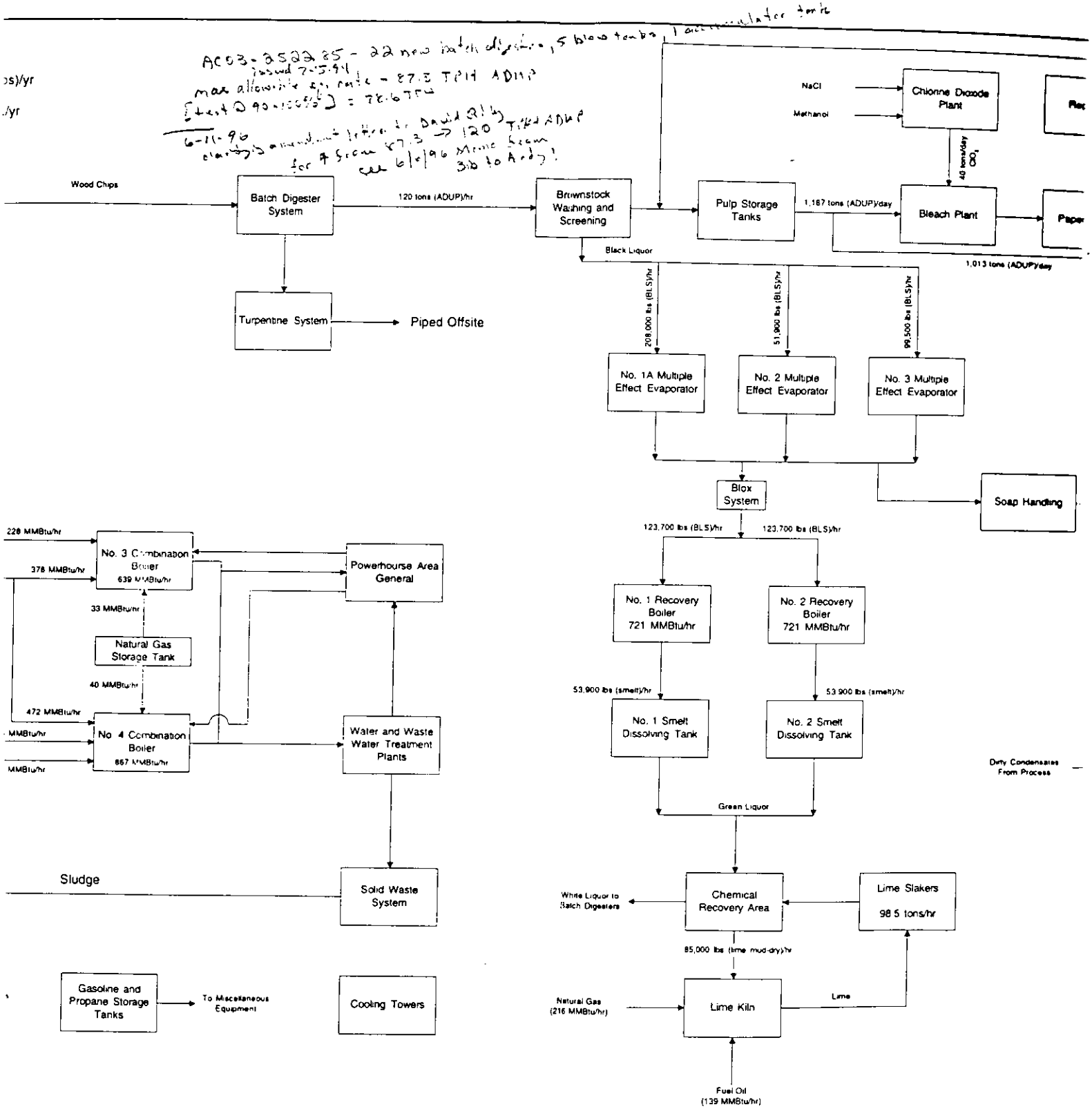

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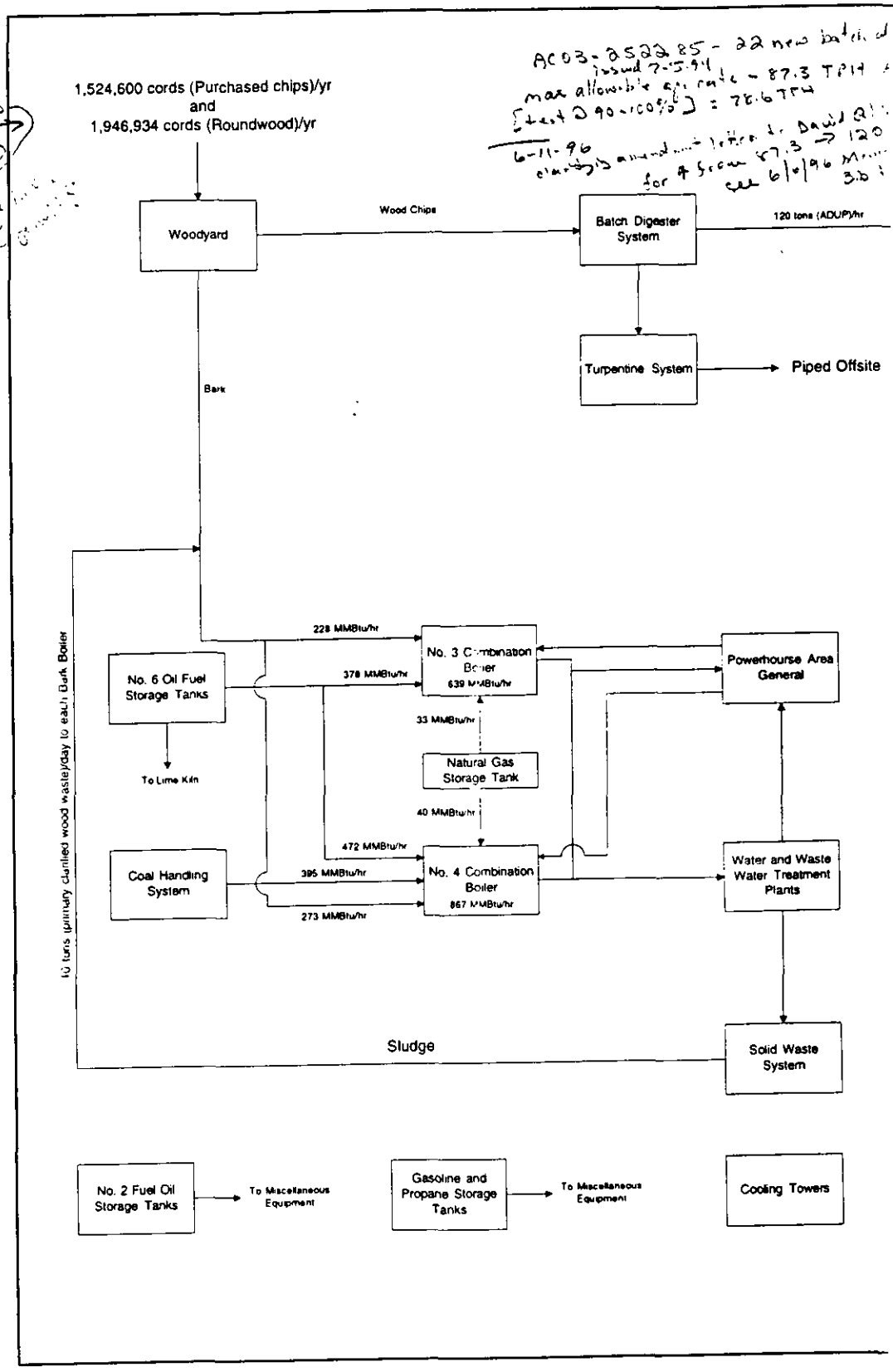

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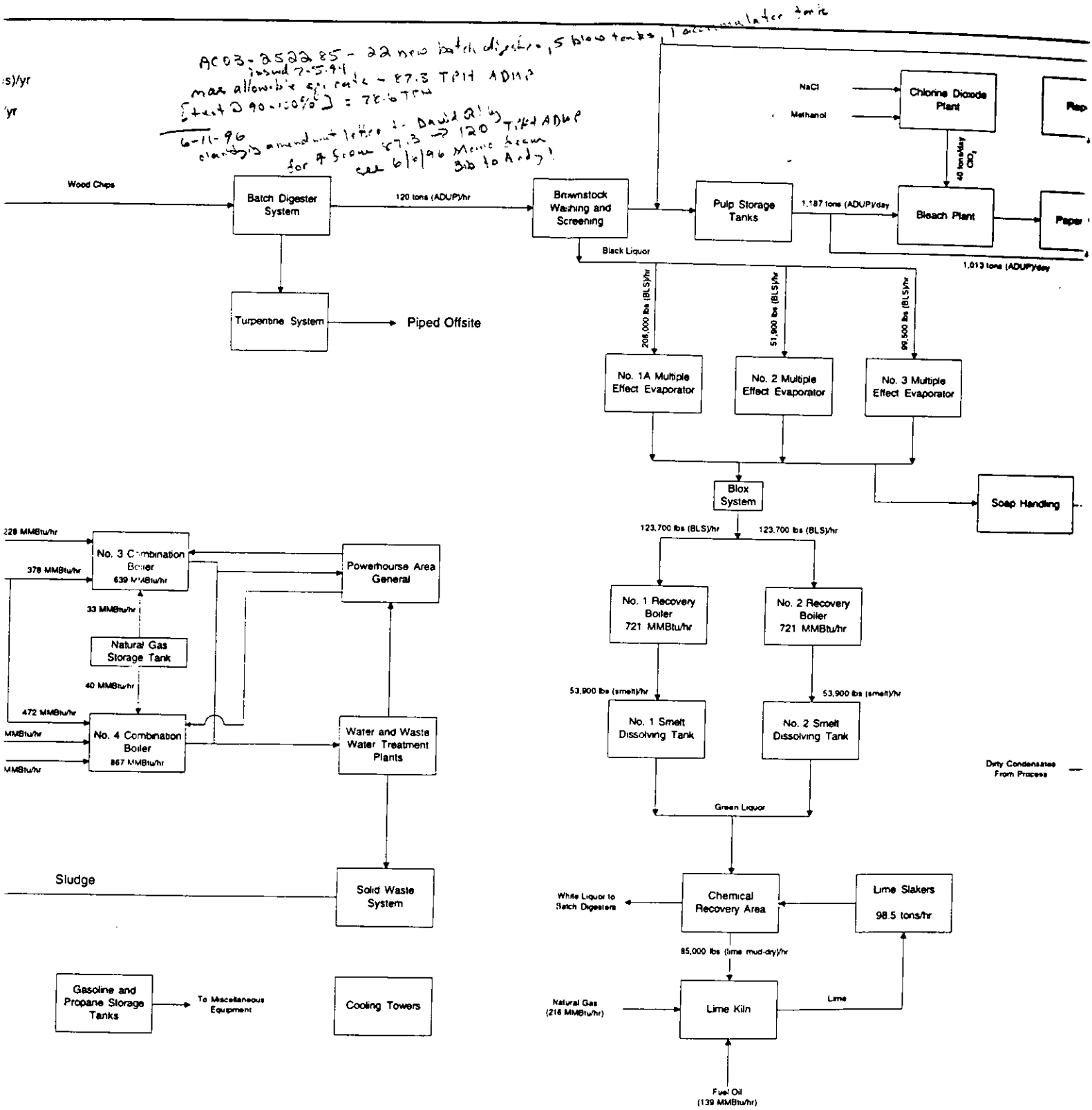
SCC-FI-C3	Panama City, FL	Filename: 9937518Y/F1/WP/SCC
		Latest Revision Date:



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	Process Area: Overall Plant Flow Diagram	
Panama City, FL	Filename: 9937518Y/F1/WP/SCC-FAC.VSD	
	Latest Revision Date: 4/5/00 4:01 PM	

BACT Applicability at Facilities Undergoing Modification

I have reviewed our rules and all available documents relating to PSD applicability and BACT review for facilities undergoing a modification. The majority of the information suggests that PSD applicability and BACT applicability can be different when reviewing modifications to existing facilities.

If a new or modified emissions unit allows for increased operation (either a higher production rate or an increase in the number of operating hours) for a unit upstream or downstream, all collateral emissions increases, in conjunction with any contemporaneous emission increases and decreases where netting is used, must be included in determining whether or not the modification is subject to PSD review (does the increase in emissions of a single air pollutant exceed the significant emission rate for that pollutant?).

A "major" modification shall apply BACT for each pollutant subject to PSD. BACT shall apply only to each proposed emissions unit at which a net emissions increase would occur as a result of the physical change or change in the method of operation.

If there are federally enforceable (construction permit after 1/6/75, FESOP, or Title V) permit conditions limiting production rate or hours of operation, changes in these conditions would constitute a modification (change in the method of operation) and could result in BACT for those emissions units.

Actual emissions are generally considered to be the average rate, in tons per year, actually emitted during a two-year period (consecutive twenty-four months or two calendar years) prior to the submission of a complete application. If the applicant shows why a different two-year period (consecutive twenty-four hours or two calendar years) during the past five years is more representative, then the review engineer shall use that two-year period.

Clair H. Fancy
July 17, 2000

FACILITY ID	NAME	EU ID	EU DESCRIPTION	YEAR	SCC	USAGE RATE	UNIT
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1996	30700104	294732	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1997	30700104	347709	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1998	10200401	860.2	1000 Gallons Burned
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1998	10200603	36.02	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1998	30700104	228917	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1999	10200401	1124.7	1000 Gallons Burned
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1999	10200603	53.3	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	1999	30700104	333626	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	2000	10200401	1491.5	1000 Gallons Burned
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	2000	10200603	36.6	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	1	RECOVERY BOILER #1 WITH ESP	2000	30700104	284375	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODU	1996	30700106	606445	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODU	1997	30700106	689231	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODU	1998	30700106	445364	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODU	1998	39000403	4211.68	1000 Gallons Burned
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODU	1998	39000603	119.77	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODU	1999	30700106	667877	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODU	1999	39000403	7045	1000 Gallons Burned
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODU	1999	39000603	109.7	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODU	2000	30700106	601216	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODU	2000	39000403	5219	1000 Gallons Burned
0050009	PANAMA CITY MILL	4	LIME KILN BURNS LIME MUD TO PRODU	2000	39000603	302.8	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	5	LIME SLAKER	1996	30700199	606445	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	5	LIME SLAKER	1997	30700199	689231	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	5	LIME SLAKER	1998	30700199	445364	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	5	LIME SLAKER	1999	30700199	667877	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	5	LIME SLAKER	2000	30700199	601216	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	14	POWER BOILER #5 (NONE)	1996			
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1996	10200401	3323.12	1000 Gallons Burned
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1996	10200603	106.94	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1996	10200901	586	Tons Burned
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1997	10200401	3443.5	1000 Gallons Burned
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1997	10200603	97.21	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1997	10200901	149362	Tons Burned
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1998	10200401	3179.4	1000 Gallons Burned
0050009	PANAMA CITY MILL	15	BARK BOILER #3	1998	10200603	80.37	Million Cubic Feet Burned

0050009	PANAMA CITY MILL	15 BARK BOILER #3	1998	10200901	138872	Tons Burned
0050009	PANAMA CITY MILL	15 BARK BOILER #3	1999	10200401	4735	1000 Gallons Burned
0050009	PANAMA CITY MILL	15 BARK BOILER #3	1999	10200603	84.1	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	15 BARK BOILER #3	1999	10200901	206210	Tons Burned
0050009	PANAMA CITY MILL	15 BARK BOILER #3	2000	10200401	2716	1000 Gallons Burned
0050009	PANAMA CITY MILL	15 BARK BOILER #3	2000	10200602	57.8	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	15 BARK BOILER #3	2000	10200603	0	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	15 BARK BOILER #3	2000	10200901	203989	Tons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1996	10200212	60421	Tons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1996	10200401	3563.3	1000 Gallons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1996	10200603	160.02	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1996	10200901	173396	Tons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1997	10200212	77610	Tons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1997	10200401	1344	1000 Gallons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1997	10200603	145.47	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1997	10200901	122203	Tons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1998	10200212	39475	Tons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1998	10200401	2656.6	1000 Gallons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1998	10200603	120.26	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1998	10200901	127580	Tons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1999	10200212	51741	Tons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1999	10200401	4015.5	1000 Gallons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1999	10200603	60.9	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	1999	10200901	111036	Tons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	2000	10200212	66450	Tons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	2000	10200401	904.7	1000 Gallons Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	2000	10200603	47.1	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	16 BARK BOILER #4 (FLY ASH ARRESTOR &	2000	10200901	135992	Tons Burned
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FR	1996	30700104	311713	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FR	1997	30700104	343254	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FR	1998	10200401	1002.92	1000 Gallons Burned
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FR	1998	10200603	36.4	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FR	1998	30700104	216447	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FR	1999	10200401	1052.94	1000 Gallons Burned
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FR	1999	10200603	53.36	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FR	1999	30700104	334251	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FR	2000	10200401	1581.3	1000 Gallons Burned

0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FR	2000	10200603	36.7	Million Cubic Feet Burned
0050009	PANAMA CITY MILL	19 RECOVERY BOILER #2 BURNING BLS FR	2000	30700104	316841	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	20 DISSOLVING TANK #2 (DEMISTER PADS)	1996	30700105	311713	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	20 DISSOLVING TANK #2 (DEMISTER PADS)	1997	30700105	341522	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	20 DISSOLVING TANK #2 (DEMISTER PADS)	1998	30700105	216447	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	20 DISSOLVING TANK #2 (DEMISTER PADS)	1999	30700105	334251	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	20 DISSOLVING TANK #2 (DEMISTER PADS)	2000	30700105	316841	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	21 #1 SMELT DISSOLVING TANK (DEMISTEF	1996	30700105	294732	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	21 #1 SMELT DISSOLVING TANK (DEMISTEF	1997	30700105	347709	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	21 #1 SMELT DISSOLVING TANK (DEMISTEF	1998	30700105	228917	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	21 #1 SMELT DISSOLVING TANK (DEMISTEF	1999	30700105	333626	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	21 #1 SMELT DISSOLVING TANK (DEMISTEF	2000	30700105	284375	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	26 MULTIPLE EFFECT EVAPORATOR (MEE)	1996	30700103	606445	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	26 MULTIPLE EFFECT EVAPORATOR (MEE)	1997	30700103	689231	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	26 MULTIPLE EFFECT EVAPORATOR (MEE)	1998	30700103	445364	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	26 MULTIPLE EFFECT EVAPORATOR (MEE)	1999	30700103	667877	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	26 MULTIPLE EFFECT EVAPORATOR (MEE)	2000	30700103	601216	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOC	1996	30700101	606445	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOC	1997	30700107	689231	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOC	1998	30700101	445364	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOC	1998	30700107	445364	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOC	1999	30700101	667877	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOC	1999	30700107	0	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOC	2000	30700101	601216	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	27 DIGESTER SYSTEM FOR COOKING WOC	2000	30700107	0	Tons Air-dried Unbleached Pulp
0050009	PANAMA CITY MILL	30 WOODYARD FACILITY	1996	30700801	2145956	Tons of Logs Processed
0050009	PANAMA CITY MILL	30 WOODYARD FACILITY	1997	30700801	1275299	Tons of Logs Processed
0050009	PANAMA CITY MILL	30 WOODYARD FACILITY	1998	30700801	858479	Tons of Logs Processed
0050009	PANAMA CITY MILL	30 WOODYARD FACILITY	1999	30700801	1321282	Tons of Logs Processed
0050009	PANAMA CITY MILL	30 WOODYARD FACILITY	2000	30700801	1222518	Tons of Logs Processed
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1996	40700815	230	1000 Gallons Storage Capacity
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1996	40700816	230	1000 Gallons Throughput
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1997	40700815	246	1000 Gallons Storage Capacity
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1998	40700815	184	1000 Gallons Storage Capacity
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1998	40700816	184	1000 Gallons Throughput
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1999	40700815	296.6	1000 Gallons Storage Capacity
0050009	PANAMA CITY MILL	31 METHANOL STORAGE TANK	1999	40700816	0	1000 Gallons Throughput

0050009	PANAMA CITY MILL	31	METHANOL STORAGE TANK	2000	40700815	247.9	1000 Gallons Storage Capacity
0050009	PANAMA CITY MILL	31	METHANOL STORAGE TANK	2000	40700816	247.9	1000 Gallons Throughput
0050009	PANAMA CITY MILL	32	Papermaking/Warehouse	1999			
0050009	PANAMA CITY MILL	32	Papermaking/Warehouse	2000	30700401	590194	Tons Finished Product
0050009	PANAMA CITY MILL	33	Bleach plant with wet scrubber	1999			
0050009	PANAMA CITY MILL	33	Bleach plant with wet scrubber	2000	30700114	307794	Tons Air-dried Unbleached Pulp