ATTACHMENT E
Proposed Construction or Modification

1.0 INTRODUCTION

This attachment provides the rationale and protocol for the D.G. Telogia Power facility located in Telogia, Florida, to modify their Florida Department of Environmental Protection (FDEP) Air Pollution Permit (No. 0770009-004-AV) to conduct a test burn co-firing conventional biomass with creosote-treated wood. The rationale that has lead to this application for a test burn is included in **Enclosure 1**. The remainder of this attachment is related to the detailed procedures to be followed for the test burn. It is anticipated that the favorable results from this test would provide the basis to apply for a revised Title V Air Operation Permit for this facility to accommodate co-firing biomass with creosote-treated woods.

2.0 FACILITY CHARACTERISTICS

2.1 UNIT DESCRIPTION

D.G. Telogia Power, LLC, operates a 14.1 MW carbonaceous fuel-fired power plant from a single steam boiler with a capacity of 150,000 pounds of steam per hour that requires a feed rate of approximately 23 tons of wood waste per hour. The facility is fueled with biomass products that comprise a combination of waste wood, cubed paper, and peanut hulls for a rated heat input of 230 million BTU per hour. The plant operates 24 hours per day, 7 days per week, and 50 weeks per year. Particulate emissions are controlled with a multi-vane cyclone and a high efficiency

electrostatic precipitator (ESP). The facility began operation in 1986 and currently operates under FDEP Title V Permit No. 0770009-004-AV, dated March 1, 2005.

2.2 FUEL PROCESSING

The carbonaceous fuel, which includes shredded waste wood, cubed paper and peanut hulls, arrives by truck. Incoming materials are first weighed on a certified scale. Once weighed, those trucks hauling wood wastes discharge their loads via a Truck Tipper into the Fuel Yard, following which the biomass fuels are placed in inventory under a covered storage area. Those vehicles carrying paper-related fuel are directed to the Paper processing facility, where the materials are offloaded using a Bobcat. Following shredding and cubing, the finished fuels are discharged to the Fuel Yard and homogenized in inventory with the wood fuels. When fuel is required at the boiler, a front end loader is used to place the fuel on a ground-level conveyor that serves as the entry point of the fuel feed system. The feed conveyor in turn moves the material through a disc screen that segregates the material into oversize and undersize fractions. The undersize material exiting the bar screen is appropriately sized as finished fuel and is subsequently conveyed to one of five fuel feed hoppers mounted on the north side of the boiler. The oversized material leaving the disc screen is routed through a hammer mill for additional size reduction and is returned to the disc screen for size separation. This cycle assures that the boiler is fired with a "to specification fuel" so as to assure optimum combustion / minimum ash generation and unburned fuels carryover. The fuel feed hoppers at the boiler are maintained continuously full with any overflow returned by conveyor to the storage area ready re-feeding on demand.

This overfeed/reclaim process cycle provides the operator with the ability to optimize the carbonaceous fuels blend that in turn maximizes both steam production and electrical output. The amount and mix of fuel fed to the boiler is controlled by a lead operator in the Boiler Control Room. This individual's job is to manage / orchestrate the proportional feed of fuel and the over-fired air intensity to maintain proper combustion. The residual ash form combustion is periodically removed from the boiler, cyclone, and ESP and disposed in a designated area at the site.

2.3 AIR EMISSIONS CONTROL

Air emissions from the boiler are controlled by two mechanisms: 1) the maintenance of appropriate residence time and temperature in the combustion zone to assure that favorable thermokinetics destroy hydrocarbons evolving from the fuel, and 2) particulate control on exhaust gases from the boiler. Measurement of the operating temperature in the boiler indicate, on average the temperature can be maintained at 1450°F (range 1366° to 1496°F)(see Paragraph 5.3), while sustaining a production of 136,000 lbs/hr of steam. The residence time of gases in the combustion zone is on the order of ten (10) seconds. The exhaust gases exit the boiler and pass through a multi-vane cyclone and a high efficiency electrostatic precipitator (ESP) in series. The gases then exhaust through a stack 81 feet high that is equipped with appropriate sampling ports, platforms, railings and access stairs which conform with regulatory stack sampling criteria. The latest emission test of the exhaust gases was conducted in October 2004 and results showed an average particulate emission rate of 0.018 pounds/million BTU's (lbs/MBTU) and plume opacity ranging from 0 to 15 percent (%). This compares to the established permit conditions of 0.05 lbs/MBTU for particulates and 20% plume

opacity. The stack is equipped with a continuous emission monitor for opacity. Bottom ash from the boiler and fly ash from particulate control devices are collected and stored in a designated area.

3.0 REGULATORY CRITERIA

3.1 CRITERIA POLLUTANTS

This facility is permitted for only particulate matter at a rate of 11.5 lbs/hr at the maximum steam production rate and not to exceed 0.05 lb/MMBtu heat input at lesser steam production rates. Further, emissions must not exhibit over 20 percent opacity (6 minute average) except for one 6-minute period per hour of no more than 27 percent opacity.

3.2 REF: 40CFR63-PART II; NATIONAL EMISSION STANDARDS FOR HAZARDOUS AIR POLLUTANTS (NESHAPS) FOR INDUSTRIAL, COMMERCIAL AND INSTITUTIONAL BOILERS AND PROCESS HEATER (FR/VOL. 69, NO. 176/SEPT. 13, 2004)

Table 1 of Subpart DDDDD of Part 63, Item 9 lists the following criteria for emission limits and work practices for this facility:

- Particulate Matter 0.07 lb per MMBtu heat input or 0.001 lb per MMBtu heat input for selected metals.
- Hydrochloride (Hcl) 0.09 lb per MMBtu heat input
- Mercury (Hg) 9E-06 lb per MMBtu heat input

4.0 POTENTIAL EMISSIONS

Data from previous test burns has been reported for two identical boilers operated in Michigan. Similar to the Telogia Power wood-fired boiler, these systems are also rated for 230 MMBtu/hr, are equipped with multi-clones in series with an ESP, which generate 18 MW of electricity and burn a combination of treated wood and biomass. The results of three separate test burns related to the parameters specified in the regulatory criteria are summarized in **Table 4-1** below. The data represent the maximum of three measurements made during each test at each facility. The entire test data is included as **Enclosures 2, 3** and **4** of this Attachment.

Table 4-1. Emissions Data From Previous Test Burns

Data Source	Viking Energy (1994)	Viking Energy (Mar. 1997)	Viking Energy (Sep. 1997)
Test Conditions(1)	29% creosote 71% wood	100% creosote	34% creosote 66% wood
Total Energy Input (lb/MMBtu)	130	215	124
Particulate Matter (lb/MMBtu)	0.032	0.007	0.0045
Hydrogen Chloride (lb/MMBtu)	0.001	ND(2)	ND
Mercury (lb/MMBtu)	1.35E-06	4.1E-08	1.6E-07
Carbon Monoxide (ppm)	120	247	80

(1) Fuel input percent by weight
(2) No data

5.0 TEST BURN CONDITIONS

It is proposed that the test burn be conducted to provide three discrete sampling events of the system operated with the fuel input of 25% creosote-treated wood and 75% conventional biomass

feed, by weight. Details of the procedures to be followed are described below.

5.1 OPERATING SCHEDULE

The test burn will be conducted over a 30-day period with each of the three discreet sampling events conducted 7 to 10 days apart. Each sampling event will be conducted over a one-day time frame and will include three individual tests. The same procedures will be followed relative to fuel preparation, boiler operations, control of the combustion process and sampling analysis of air emissions and residual ash during each sampling event.

5.2. FUEL CONTROL, CERTIFICATION AND PREPARATION

The facility operators recognize the importance that the treated wood used in the test burn is limited to creosote-treated wood. Other types of treated wood that could be encountered include: wood treated with Pentachlorophenol (PCP), Chromated Copper Arsenate (CCA), copper-based water-borne preservative and borate. In order to assure the fuel used in the test burn is only creosote-treated wood, the following measures will be taken.

5.2.1 Bulk Treated Wood

The generator of the source of the material will be required to provide a comprehensive characterization of the waste by completing the Proprietary Waste Application for DGTP Facilities form that is included as Enclosure 5. In addition, the facility operators or representative will physically inspect the source material for its use characteristics, size, shape, color and odor of the treated wood and document this information on the facility form previously cited. In addition after arrival at the facility, a field test

using a chemical stain indicator will be conducted to confirm that inorganic metal-based wood preservatives (i.e., CCA) are not present. A minimum of three items in a bulk load will be tested (or more if warranted) after the initial physical inspection process. The stain indicator proposed is a PAN indicator whose application has been documented (Blassino, M., et al, "Sorting Technologies for CCA-treated Wood", Waste Management and Research 20:290-301 (2002)). Should the source material fail either the physical inspection or the chemical stain evaluation, the original owner will be responsible to recover and properly dispose of the rejected material.

5.2.2 Sized Reduced Treated Wood

Should the source treated wood arrive at the facility in a sized reduced form, in addition to the source information required on the form (Enclosure 5), the source of the treated wood will be required to provide a confirmation analysis of the product. A representative sample of the material will be collected (in triplicate) and analyzed. The analysis will consist of a synthetic precipitation leaching procedure (SPLP, EPA Method 1312) measuring the concentration of chromium, copper and PCP in the leachate using EPA Methods and a certified laboratory. The material will be segregated and staged until such time as the analytical data confirms the material acceptable for the trial burn. If the material is not acceptable, the original owner of the source material will be responsible to remove the material and arrange for its proper disposal.

The methods described heretofore should provide significant confidence at the regulatory level that the treated wood used in the test burn is limited to that only treated with creosote.

The results of these procedures will be included in the test burn final report.

Finally, the treated wood and conventional biomass will be mixed in proportions required for the test burn, on a weight basis, using a front-end loader. Such "test bound" materials will be stored under cover until such time as they are used in the test burn proper.

5.3 BOILER OPERATIONS

Prior to initiating a test event, the boiler will be brought up to operating temperature (1400-1500°F) with conventional biomass. After reaching operating temperature, the boiler feed hopper will be charged with the previously prepared proportional mixture of creosote-treated wood and biomass. The boiler will be operated over a period of one-hour to stabilize the feed of the proportional mixture of fuel (nominally 17 tons/hr of biomass and 6 tons/hr of creosote-treated wood), during which bottom ash will be removed from the boiler and fly ash from the air pollution control systems. After stabilizing the fuel feed to the system, a series of three, one-hour air emission sampling tests will be initiated and completed. At the conclusion of the three sampling events, residual ash will be sampled for analysis.

Operational control of the boiler during the tests will be monitored to assure the appropriate over-fire air and temperatures are optimized for combustion. Thermokinetic modeling to achieve destruction of any air toxics is projected to be on the order of 1100°F (see **Enclosure 6**). To assure the process combustion is effective, should the temperature fall to 1300°F, the co-firing with the mixed fuel will be terminated and the feed to conventional

carbonaceous fuel will be resumed to sustain the appropriate operating temperature (nominally 1400°F).

5.4 AIR EMISSIONS SAMPLING/ANALYSIS

Emission testing during each event will conform to the conduct of sampling and analysis as specified in Section III, Test Methods and Procedures (Section A.7) outlined in this referenced FDEP permit for this facility. In addition to those testing procedures, sampling protocols for air toxics will be followed to include; EPA Method 23 (dioxin/furans and PAH), Method 25A (total hydrocarbons), Method 26A (particulate matter and HCL), Method 29 (Metal HAPs), Method SW-846 M0011 (aldehydes and ketones), and Method SW-846 M0030 (volatile organics sampling train). Conventional well proven procedures will be followed for method blanks, field blanks, etc., in the approved QA/QC sampling plan. Note that the parameters to be evaluated in this test are significantly greater than those prescribed by U.S. Environmental Protection Agency (USEPA) criteria for this facility (see Paragraph 3.2).

Subsequent to collection of the data from each stage, an ambient air impact analysis will be performed using air dispersion models to assess both the potential ambient air levels of exposure to the emissions in proximity to the facility.

5.5 FUEL AND RESIDUAL ASH SAMPLING/ANALYSIS

The co-fired fuel will be sampled for each event in proportion to representative weight to determine its ultimate and proximate values including; heating value, and percent by weight of hydrogen, total carbon, fixed carbon, nitrogen, volatiles, ash, oxygen, sulfur, and chlorine.

After each event, the bottom and fly ash will be sampled and analyzed using the toxic characteristic leaching procedure (TCLP) for all the constituents listed in the RCRA TCLP Hazardous Waste regulatory levels. Sampling will combine the two ashes in an equal quantity, mixed thoroughly and sequentially quartered until approximately one pound is retained for analysis. Again, an independent certified laboratory will perform the analysis and the appropriate QA/QC protocol will be followed. The bottom and fly ash generated during the test burn will be collected, segregated and placed in covered storage until analytical results from hazardous waste have been completed. The ash will then be disposed consistent with regulatory criteria.

ATTACHMENT E

Enclosure 5

Material Management Plan

1. **Introduction.** This plan lays out the details in handling for the solid fuel material used during the test burn to charge the boiler and the evaluation of ash residual after the material has been fired in the boiler. The test burn will be conducted at the permitted fuel feed rate of 23 tons/hr with fuel consisting of 75% conventional biomass (CB) and 25% creosote-treated wood (CTW), by weight. The sampling and analysis of the fuel follows the guidelines outlined in 40 CFR Part 63.7520 and 63.7521 published in the Federal Register/Volume 69, No. 176, September 13, 2004/Rules and Regulations, where appropriate.
2. **Fuel Source.** The proposed source of the CTW is railroad ties procured in their existing physical condition from Florida East Coast R/R and/or Florida Central R/R. The total mass of CTW to be processed during the 24 hours required for the trial burn is appropriately 140 tons and 415 tons of CB. The size range of the combined material to fuel the boiler will be ≤ 6 inches. The CTW will be processed to that size range at the originating site prior to transport to Telogia.

   The source of the proposed CTW is to be creosote-treated scrap railroad ties currently stockpiled at one of the following facilities:

   1) Florida East Coast R/R yard in Fort Pierce, Florida and
   2) Florida Central R/R in Orlando, Florida.

   The total mass of CTW to be processed during the 24-hours required for the trail burn is approximately 140 tons. Approximately 415 tons of CB will be processed at the same time to achieve to appropriate 3:1 ratio of CB/CTW.
3. **Screening Incoming CTW**. All CTW will be physically processed for transfer to Telogia at the originating source (i.e. Ft. Pierce, Orlando sites). The following steps will be taken in processing and testing the CTW prior to shipment to the Telogia Facility:

   a) Proposed material will be physically identified, located on the property, and photographed.
   b) The R/R ties identified for the trial burn will then be inspected and have any miscellaneous material – metal spikes, nails, wire, other wood products, etc. – removed and separated from the CTW.
   c) The CTW will be physically processed at the originating site, i.e. chipped via tub grinder or other suitable method that will attain the desirable ≤6-inch size prior to transfer to Telogia facility.
   d) Workers involved with the handling of the CTW shall meet, at the minimum, the conditions of the Health and Safety Assessment set forth in Item #10 of this Plan.
   e) The physically processed CTW will be sampled following the regulatory total selected metals (TSM) (lb/MMBtu) (TSM includes As, Be, Cd, Cr, Pb, Mn, Ni, Se). A minimum of

three (3) composite samples will be taken of CTW pile using the method described as follows:

- For each composite sample, five (5) sampling locations uniformly spaced over the surface of pile shall be selected. At each sampling site a hole shall be dug to a depth of 18-inches. A clean, flat square shovel shall be inserted into the hole to withdraw a sample. Sampler shall make sure that large pieces do not fall off during sampling.
- Samples shall be identified and transferred to a clean plastic bag until further processing.
- The entire sample is then mixed and poured over a clean plastic sheet where pieces larger than three (3) inches are broken to smaller sizes.
- The sample material is then formed into a pie shape, subdivided into four equal parts, one of the quarters separated and the sample ground in a mill.
- The ground sample is then identified and placed in a clean plastic bag and submitted to a laboratory for analysis.

This procedure is repeated to obtain the representative three (3) composite samples for analysis.

NOTE: If more than one site, i.e. Ft. Pierce/Orlando, is used to supply the CTW, then material from each site shall be sampled accordingly.

Ref. Fed. Reg., Vol 69, No 176, 9/13/04, Rules and Regulations. All sampling will be performed by independent laboratory personnel.

4. **Laboratory Testing Results of Source CTW:** Results of laboratory tests of the CTW source material will be forwarded to FDEP for confirmation prior to shipment from the source. A chain of custody shall be established to assure responsibility of transport and proper receipt of the CTW by Telogia. A record shall be kept of the quantity of CTW leaving the site and receipt of same at Telogia.
5. **Receipt of CTW at Telogia:** All transports carrying CTW to Telogia shall be logged in and weighed. Transports shall be directed to the truck lift where the CTW will be deposited and then moved by loader to its staging area. The staging area as shown on the accompanying figure is isolated from the other CB fuel storage areas.
6. **Blending of the CB and CTW.** For each of the 3 test burns, the sized CB and CTW will each be sampled three times with a full bucket on a front end loader, weighted and the average weight of a bucket load determined. Following this procedure, the front end loader will load a proportional quantity of the CB and CTW at an area in the vicinity of the conveyers. The blended fuel pile will then be mixed by manipulating the pile with the front end loader until relatively homogenous. The mixed material will then be loaded onto a conveyor that routes the fuel to the boiler feed chute. The mixed material is sampled on the conveyor belt following regulatory guideline procedures described below.
7. **Sampling and Analysis of the Blended Fuel.** The analysis performed will be the same as detailed in Paragraph 3, above. The sampling of the fuel from the belt will include three composite samples at approximately three equal intervals during the course of each of the test burns. Each sample will be taken while the belt is stopped and a six-inch wide sample from the full cross section of the belt will be taken to obtain a minimum sample of two pounds (including fines and coarse material). The sample will be transferred to a clean plastic bag, identified properly, and submitted for analysis.

8. **Sampling and Analysis of Ash Residue.** Sampling of residual ash in the boiler and electrostatic participator (ESP) will be conducted at approximately three equal intervals during each of the three 8-hour test burn sequences. Approximately one pound of ash will be extracted from the boiler grate and the ESP, allowed to cool, mixed and placed/identified in a clean plastic bag. Each of the three samples will be analyzed using the toxic characteristic leaching procedure (TCLP) for the potential hazardous waste constituent regulatory levels.
9. **Storage and Final Disposal of Ash:** All ash, boiler and ESP, created during the test burn, will be segregated and stored in covered 30-yard roll off containers until analyzed and cleared for deposing in Telogia's ash disposal landfill. If the ash does not meet regulatory requirements for disposal at Telogia's facility, then it will be transported to a site permitted to receive ash of the characteristics listed in the laboratory analysis.
10. **Health and Safety Assessment:** Coal tar creosote was formerly used to treat railroad ties and contains a mixture of polycyclic aromatic hydrocarbons (PAHs) and volatile organic compounds. This health and safety assessment recommends precautions that should be implemented for the prevention of exposure to hazards associated with the grinding and handling of creosote treated railroad ties. Care should be taken during the grinding/hauling of railroad ties to prevent both dermal and ocular exposure as well as inhalation and ingestion of creosote containing wood sawdust and particulate. Noise exposure levels during operation of grinding equipment should be measured to assure proper hearing protection of workers.

    a) Protective Clothing and Personal Protective Equipment (PPE)
    Protective clothing and eye protection including eye goggles, face shields, disposable Tyvek suits, and gloves that are impervious to chemicals should be worn to prevent contact of creosote-treated wood and wood particulate with eyes and bare skin. A respirator should be worn to prevent inhalation and/or ingestion of particulate sawdust from grinding of creosote-treated wood and should include organic vapor protection.

    b) Personnel Monitoring
    The grinding, process of creosote-treated railroad ties, mixing with CB and feeding mixed fuel to conveyors creates potential exposure to wood particulate, or nuisance dust, respirable dust particules, and polycyclic aromatic hydrocarbons and volatile organic compounds. The Occupational Safety and Health Administration (OSHA) recommends sampling for phenol, cresols, naphthalene, and coal tar volatile compounds associated with creosote as exposure indicators. Substances to be monitored and their associated OSHA Permissible Exposure Limits are listed in **Table 1** below.

Table 1. Substances to be Monitored and Associated PEL's

Monitored Substance	OSHA PEL based on an 8-hour Time Weighted Average (TWA)
Total Wood (Nuisance) Dust	15 mg/m^3
Respirable Dust	5 mg/m^3
Phenol	19 mg/m^3
Cresol	22 mg/m^3
Napthalene	50 mg/m^3
Coal Tar Pitch Volatiles	0.2 mg/m^3

c) Noise Exposure Level Monitoring

Noise level exposure of workers during the grinding process should be monitored to assure that daily allowable noise dose levels are not exceeded. Exposure time limits and the associated OSHA Permissible Exposure limit are listed in **Table 2** below.

Table 2. PEL's and Maximum Exposure Times for Noise

Exposure	OSHA PEL (Decibels)
8	90 dB
4	95 dB
2	100 dB
1	105 dB
0.5	110 dB
0.25	115 dB

It is recommended that qualified personnel provide an onsite health and safety assessment to include personnel monitoring of workers for particulate and chemical exposure and to conduct noise level exposure monitoring.

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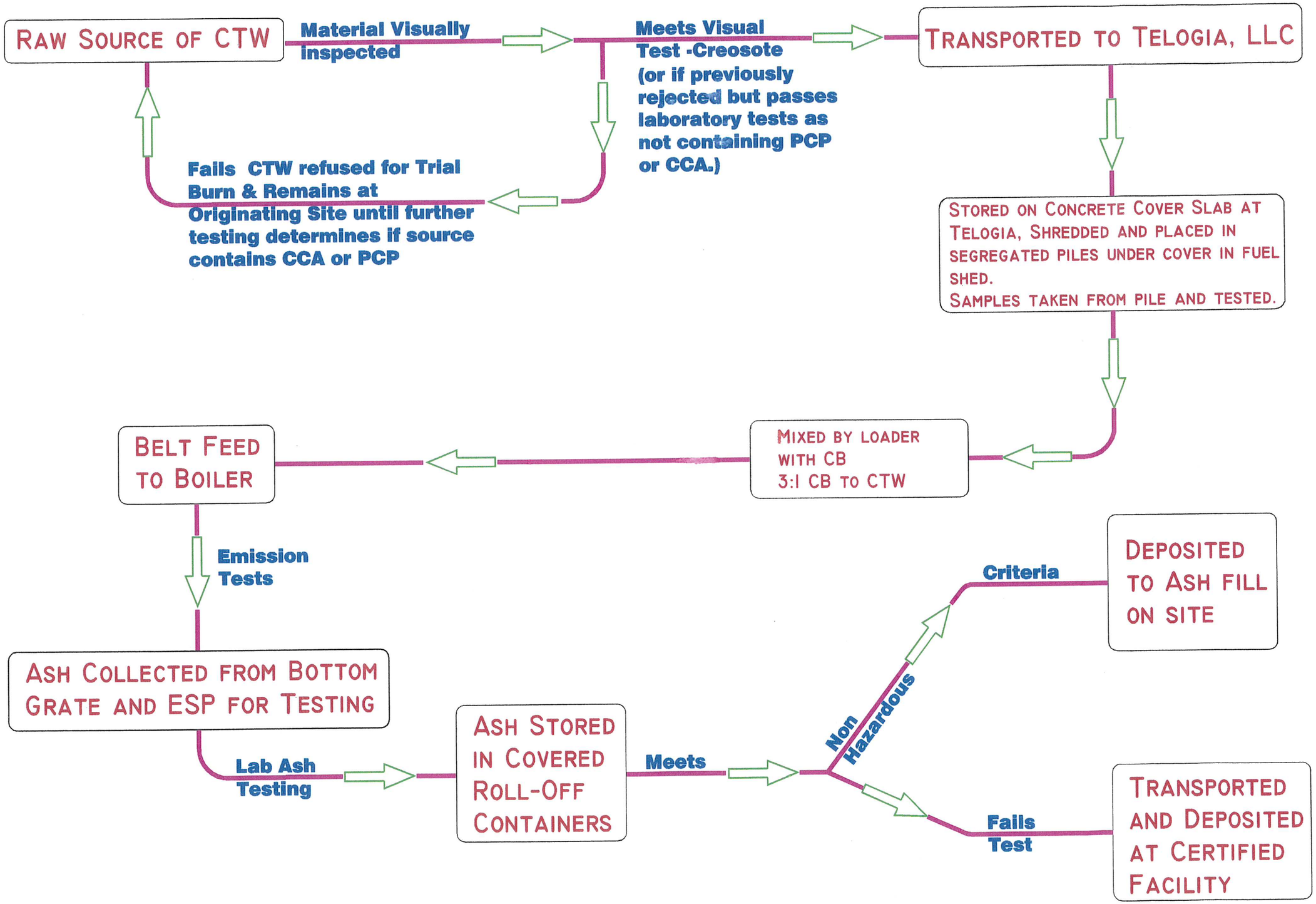

Rev: 2-8-07

Figure 1

engineers – architects – surveyors – scientists

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Atlanta Lakeland Orlando Sebring Tallahassee Tampa

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REVISED DATE	
2-8-07	Revised some Text

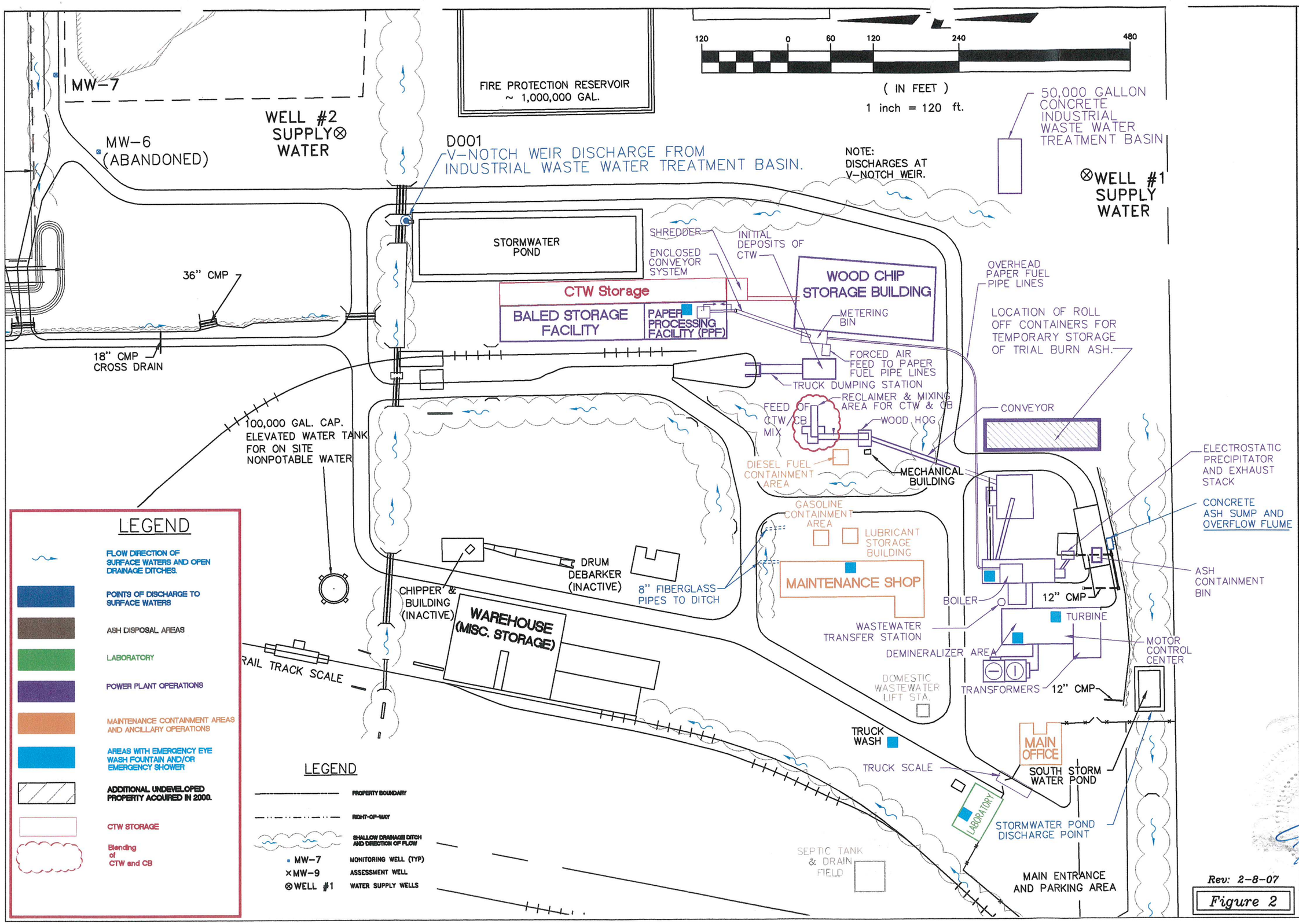
120 0 60 120 240 480
(IN FEET)
1 inch = 120 ft.
FIRE PROTECTION RESERVOIR ~ 1,000,000 GAL.
MW-7
WELL #2 SUPPLY WATER
MW-6 (ABANDONED)
D001 V-NOTCH WEIR DISCHARGE FROM INDUSTRIAL WASTE WATER TREATMENT BASIN.
NOTE: DISCHARGES AT V-NOTCH WEIR.
50,000 GALLON CONCRETE INDUSTRIAL WASTE WATER TREATMENT BASIN
WELL #1 SUPPLY WATER
STORMWATER POND
36" CMP
18" CMP CROSS DRAIN
SHREDDER
INITIAL DEPOSITS OF CTW
ENCLOSED CONVEYOR SYSTEM
CTW Storage
BALED STORAGE FACILITY
PAPER PROCESSING FACILITY (PPF)
WOOD CHIP STORAGE BUILDING
METERING BIN
OVERHEAD PAPER FUEL PIPE LINES
LOCATION OF ROLL OFF CONTAINERS FOR TEMPORARY STORAGE OF TRIAL BURN ASH.
FORCED AIR FEED TO PAPER FUEL PIPE LINES
TRUCK DUMPING STATION
RECLAIMER & MIXING AREA FOR CTW & CB
FEED OF CTW CB MIX
WOOD HOG
CONVEYOR
DIESEL FUEL CONTAINMENT AREA
MECHANICAL BUILDING
ELECTROSTATIC PRECIPITATOR AND EXHAUST STACK
100,000 GAL. CAP. ELEVATED WATER TANK FOR ON SITE NONPOTABLE WATER
GASOLINE CONTAINMENT AREA
LUBRICANT STORAGE BUILDING
CONCRETE ASH SUMP AND OVERFLOW FLUME
MAINTENANCE SHOP
DRUM DEBARKER (INACTIVE)
8" FIBERGLASS PIPES TO DITCH
CHIPPER & BUILDING (INACTIVE)
WAREHOUSE (MISC. STORAGE)
BOILER
12" CMP
TURBINE
ASH CONTAINMENT BIN
WASTEWATER TRANSFER STATION
DEMINERALIZER AREA
MOTOR CONTROL CENTER
RAIL TRACK SCALE
DOMESTIC WASTEWATER LIFT STA.
TRANSFORMERS
12" CMP
TRUCK WASH
MAIN OFFICE
TRUCK SCALE
SOUTH STORM WATER POND
LABORATORY
STORMWATER POND DISCHARGE POINT
SEPTIC TANK & DRAIN FIELD
MAIN ENTRANCE AND PARKING AREA
LEGEND
FLOW DIRECTION OF SURFACE WATERS AND OPEN DRAINAGE DITCHES.
POINTS OF DISCHARGE TO SURFACE WATERS
ASH DISPOSAL AREAS
LABORATORY
POWER PLANT OPERATIONS
MAINTENANCE CONTAINMENT AREAS AND ANCILLARY OPERATIONS
AREAS WITH EMERGENCY EYE WASH FOUNTAIN AND/OR EMERGENCY SHOWER
ADDITIONAL UNDEVELOPED PROPERTY ACQUIRED IN 2000.
CTW STORAGE
Blending of CTW and CB
LEGEND
PROPERTY BOUNDARY
RIGHT-OF-WAY
SHALLOW DRAINAGE DITCH AND DIRECTION OF FLOW
MW-7 MONITORING WELL (TYP)
MW-9 ASSESSMENT WELL
WELL #1 WATER SUPPLY WELLS
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Figure 2
engineers - architects - surveyors - scientists
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Revised CTW Storage Area
2-8-07
REVISED DATE
R-1
REVISION NO.
DRAWN BY CDT
REV. P#
DATE 05-08-06
SCALE NTS
Construction Permit Application For Telogia Power, LLC
CTW and Ash Storage For Trial Burn
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2/14/07
ENGINEER: Pearce L. Barrett III, P.E.
REG. NO. 35464
DRAWING NO.
CSI 8840.01 2