RECEIVED

HUMAN CREMATORY AIR GENERAL PERMIT REGISTRATION FORM

JAN 3 0 2012

Part II. Notification to Permitting Office

DIVISION OF AIR RESOURCE MANAGEMENT

(Detach and submit to appropriate permitting office; keep copy onsite)

Instructions: To give notice to the Department of an eligible facility's intent to use this air general permit, the owner or operator of the facility must detach and complete this part of the Air General Permit Registration Form and submit it to the appropriate Department of Environmental Protection or local air pollution control program office which has permitting authority. Please type or print clearly all information, and enclose the appropriate air general permit registration processing fee pursuant to Rule

62-4.050, F.A.C. (\$100 as of the effective da	e of this form)	4427
Registration Type		7761
Check one:	, , ,	
INITIAL REGISTRATION - Notification of a Construct and operate a proposed new facil Operate an existing facility not currently us air operation permit to an air general permit	ty. ng an air general permit (e.g., a faci	lity proposing to go from an
RE-REGISTRATION (for facilities currently to Continue operating the facility after expirate Continue operating the facility after a change Make an equipment change requiring re-reg other change not considered an administration	on of the current term of air general e of ownership. stration pursuant to Rule 62-210.31	permit use. 0(2)(e), F.A.C., or any
Surrender of Existing Air Operation Permit(s)	For Initial Registrations Only	
If the facility currently holds one or more air operator operator upon the effective date of this air gener operation permits being surrendered. If no air operation permits being surrendered.	al permit. In such case, check the fination permits are held by the facility	rst box, and indicate the v, check the second box.
All existing air operation permits for this fac general permit; specifically permit number(s		effective date of this air
No air operation permits currently exist for the	is facility.	· ·
General Facility Information		
<u>Facility Owner/Company Name</u> (Name of corporat operates, controls, or supervises the facility.)	on, agency, or individual owner who	o or which owns, leases,
Lew Hall/ Gentry Morrison	'uneral Home	
Site Name (Name, if any, of the facility site; e.g., P owned, a registration form must be completed for e	ant A, Metropolis Plant, etc. If morch.)	e than one facility is
Gentry Morrison Funeral Ho	ıe	
Facility Location (Provide the physical location of t	e facility, not necessarily the mailir	ng address.)
Street Address: 1813 Richmond Road City: Lakeland County	Polk Zip Co	de: 33801 – 2541
Facility Start-Up Date (Estimated start-up date of pr	posed new facility.) (N/A for existing	ng facility)
April 2012		
-		

DEP Form No. 62-210.920(2)(c) Effective: January 10, 2007

Owner/Authorized Representative

Name and Position Title (Person who, by signing this form below, certifies that the facility is eligible to use this air general permit.)

Print Name and Title:

Lew Hall, Owner

Owner/Authorized Representative Mailing Address

Organization/Firm: Gentry Morrison Funeral Home

Street Address: 1833 S. Florida Ave.

City: Lakeland

County: Polk

Zip Code: 33803

Owner/Authorized Representative Telephone Numbers

Telephone: 863-688-7679

Cell phone (optional):

Fax: 863-683-4167

Facility Contact (If different from Owner/Authorized Representative)

Name and Position Title (Plant manager or person to be contacted regarding day-to-day operations at the facility.)

Print Name and Title:

Same as Above

Facility Contact Mailing Address

Organization/Firm:

Street Address:

City:

County:

Zip Code:

Facility Contact Telephone Numbers

Telephone:

Fax:

Cell phone (optional):

Owner/Authorized Representative Statement

This statement must be signed and dated by the person named above as owner or authorized representative

I, the undersigned, am the owner or authorized representative of the owner or operator of the facility addressed in this Air General Permit Registration Form. I hereby certify, based on information and belief formed after reasonable inquiry, that the facility addressed in this registration form is eligible for use of this air general permit and that the statements made in this registration form are true, accurate and complete. Further, I agree to operate and maintain the facility described in this registration form so as to comply with all applicable standards for control of air pollutant emissions found in the statutes of the State of Florida and rules of the Department of Environmental Protection and revisions thereof.

I will promptly notify the Department of any changes to the information contained in this registration form.

Signature

/2/3//// Date

DEP Form No. 62-210.920(2)(c) Effective: January 10, 2007

Design Calculations

If this is an initial registration for a proposed new human crematory unit, provide design calculations to confirm a sufficient volume in the secondary chamber combustion zone to provide for at least a 1.0 second gas residence time at 1800 degrees F.

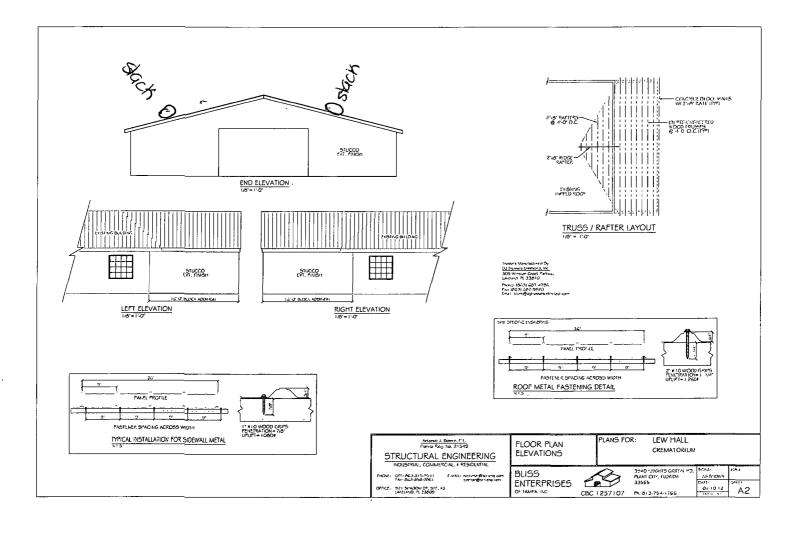
Manufacturer's' design calculations attached.

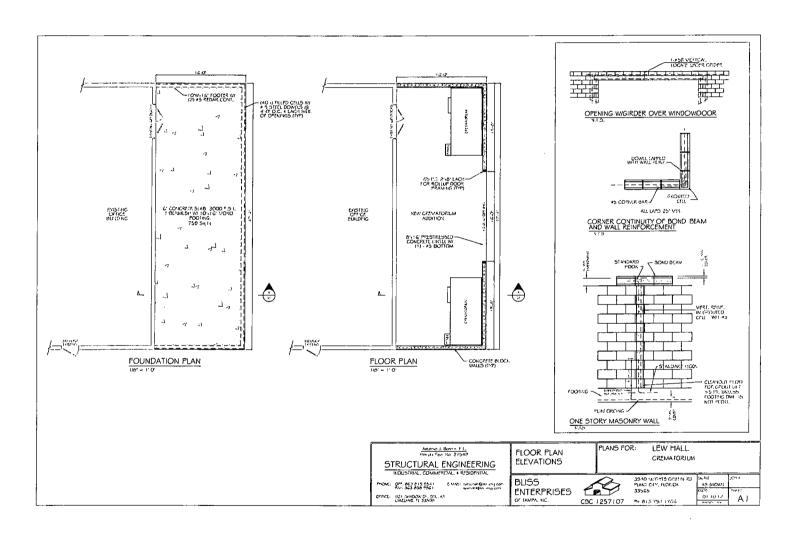
Registration is not for proposed new human crematory unit(s).

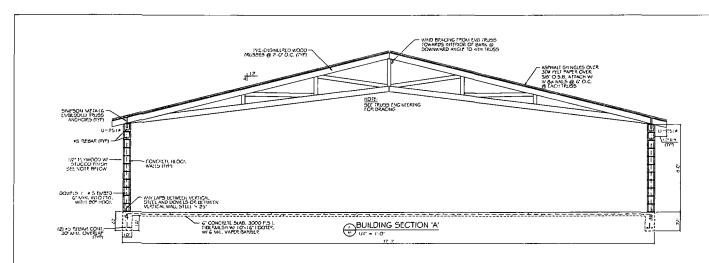
Description of Facility

Below, or as an attachment to this form, provide a description of all crematory operations at the facility in sufficient detail to demonstrate the facility's eligibility for use of this air general permit and to provide a basis for tracking any future equipment or process changes at the facility. Describe all air pollutant-emitting processes and equipment at the facility, and identify any air pollution control measures or equipment used.

Funeral Home and crematory operating a B&L Cremation Systems, Inc. Human crematory with internal afterburner with a minimum of a one second retention time at 1800°F.







GENERAL NOTES:

- F. THE BUILDING IS IN ACCOPDANCE WITH 2007 PLOFIDA BUILDING CODE
- 2. BASIC WIND SPLED = 120 VPH
- 3. EXPOSURE CATEGORY: B 4. INPORTANCE FACTOR: .77
- 5. ALL WOOD IN THIS STRUCTURE TO BE SP #2 GRADE OR BETTER.
- 6. ANCHOPED TO SOIL BASED ON FOUNDATION DESIGN EP-486 PER ASAE (AVERICAN SOCIETY OF AGRICULTURAL ENG.)
- FOR STRUCTUPAL INTEGRITY, METAL SHELTING SHALL BE MINIMUM STANDARD 29 GA., 50,000 LB, TENSILE STRENGTH.
- B. DESIGN WIND PRESSURE FOR EXTERIOR COMPONENTS AND CLADDING (-7-) 30 PSF. 9. INTERNAL PRESSURE COEFFICIENT - ENCLOSED (+1-) 0.18.
- RETENTIO

200 CL 1 CL 11 CD 1011112	E. STALL DE TOLLOWS.
ON (LBS/CU.FT)	USES/EXPOSURE
.25	ABOVE GROUND
.40	GROUND CONTACT
	FRESH WATER
.GO	WOOD FOUNDATION
2.50	SALT WATER

- 11. ALL DODGE, WINDOWS & ROOPING/FIDING MATERIALS TO BE INSTALLED AS TRE MATERIAC TURES INSTRUCTIONS. INVISES OFFICEMES STATE! CONTRACTOR OR OWNER SHALL SUPPLY VEXDOR DATA STATING THE ADOVE LENGE, COUNSY WITH 2007 FLORIDA BUILDING CODE FOR 120 MITH WINDS.
- 12. ELECTRICAL, PLUMBING & INVAC IN REQUIRED FOR THIS PROJECT WILL BE PERFISHED AT A LATER DATE.
- 13. SIDEWALL OR GABLE METAL PASTENED @ 910 C. HORIZONTAL AND 241 O.C VERTICAL.

NAILING SCHEDULE (AS NELDED)		
14th	RAILING	ALIOWABLE UP(IFT (LBS)
SIMPSON METALE	9-10-11 1/2 NALS	1450
SIMPSON HI	6-8-1 NALS	490
5'MP50N HT0	8-8a NAUS	905
5'MP50N HT512	12-10a NAUS	775

Actomo J. Dennin, F.E. Flanda Reg. No. 21549

STRUCTURAL ENGINEERING

PRONE OFF AGE-015-05-41 F MAIL restymer@ve-drg.com FAR 063-030-0061 scorolo@strates.com Office: 921 58400W09, 512, 43 (A/2) 490, 11 3350%

BUILDING SECTION

PLANS FOR: LEW HALL CREMATORIUM

BLISS ENTERPRISES OF LAMPA, INC.

CBC 1257107

AS SHOWN

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Sec.: 28 Twp.: 28 S. This Boundary S	on 01 / 02 / 12 Fil		
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These docum intellectus	ents and all data and/or information depicted shall remain the sole Professional property of M. Stewart McDonald until the Professional fee is paid in full.		
	l property of M. Stewart McDonald until the Professional Ice is paid in full. Copyright © 2012 by M. Stewart Mc Donald - P.L.S. All rights reserved.	16,9	
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Por	M.C. Markett D. C. D. C. M. C.	RANG MAN EQUIN	
	M. Stewart McDonald - Florida Professional Land Surveyor # 5919 Mailing Address: P.O. Box 616 - Knthleen, FL 33849-0616 Office Address: 3318 Scenic Way - Lakeland, FL 33810-2665	Store went U.S. 98 SOUTH	
This Sketch is not be wasted not past in full as is not	PH # (863) 853-9100 FAX (863) 853-9300 valid without the signature & original ratiod seal of 51 Newson McDonald, F.P.L.S. No. 5919. Additions and/or deletions to the	1, 0,	
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*Wind Direction is generally from the West

CALCULATIONS FOR PRODUCTS OF COMBUSTION AND RESIDENCE TIME FOR 150 LB/hr TYPE IV WASTE. B&L N-20 SERIES CREMATORY

PROPANE

A. BASIS: 1 LB WASTE

1. <u>1 lb waste X 1000 Btu/lb waste X 15 lbs air</u> = 1.5 lbs air 10,000 Btu

2. 1 lb waste \times 0.10 lb combustible = 0.10 lbs of combustibles

1 lb waste

3. 1 lb waste X 0.85 lb H20 X 1.6* = 1.36 lbs of water

1 lb waste

4. 6,500 Btu aux fuel** X 23.8 cu ft air/cu ft fuel = 4.64 lbs of air for aux fuel

2,500 Btu/cu ft fuel X 13.35 cu ft air/lb air @ 70f

5. 6,500 Btu aux fuel \times 0.044 lb fuel/cu ft fuel = 0.11 lb of aux fuel

2,500 Btu/cu ft fuel

6. Sum = PRODUCTS OF COMBUSTION (POC) = 7.71 lbs POC per lb

waste @ 70f

B. RESIDENCE TIME @ 1600 F

1. <u>7.71 lbs POC/lbs waste X 51.89 cu ft / lb POC @ 1600f X 150 lbs waste / hr</u> 3600 sec/hr

= 16.67 cu ft / sec @ 1600 f = 17.00 cu ft for 1 second residence time

RESIDENCE TIME @ 1800 F

2. 7.71 lbs POC/lbs waste X 56.93 cu ft / lb POC @ 1800f X 150 lbs waste / hr 3600 sec/hr

= 18.1 cu ft / sec @ 1800 f = 19.00 cu ft for 1 second residence time

* Correction multiplier for dry air and water vapor

** Fuel is propane

Referances: Incinerator institute of America.

North American Combustion Handbook Eclipse Combustion Engineering guide

C. THERMOCOUPLE PLACEMENT.

Secondary chamber operating temperature at > or = to 1600f = 17.00 cu ft from flame tip. 1800f = 19.00 cu ft from flame tip.



Systems, Inc.

7205 - 114th Avenue North • Largo, Florida 33773 1-800-622-5411 • 727-541-4666 • Facsimile 727-547-0669

PROCESS DESCRIPTION

This project consists of the construction of one new cremation retort. This crematorium will consist of one B & L Systems Model N-20AA Human Cremator. The cremation unit will be fired on propane.

Deceased human remains are manually placed into the primary chamber of the cremator. The door of the cremator is then closed. After a preheat of the afterburning chambers by the auxiliary burner, initial and supplementary combustion is provided by a propane fired burner located in the primary chamber of the cremator. Once material combustion is initiated, the rate of the combustion is controlled by limiting both the combustion air and fuel supplied to the primary chamber through the primary burner. This process generates a highly combustible gas mixture that flows into a secondary chamber where more air is admitted to insure further oxidation of the gases. The auxiliary burner is installed in the secondary chamber of the cremator to facilitate complete combustion of all gaseous materials entering this chamber.

Once the cremation process is complete, the remains are removed from the primary chamber of the cremator. These remains are placed in urns and returned to the family for interment of disposal.



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TEMPERATURE CONTROL SEQUENCE

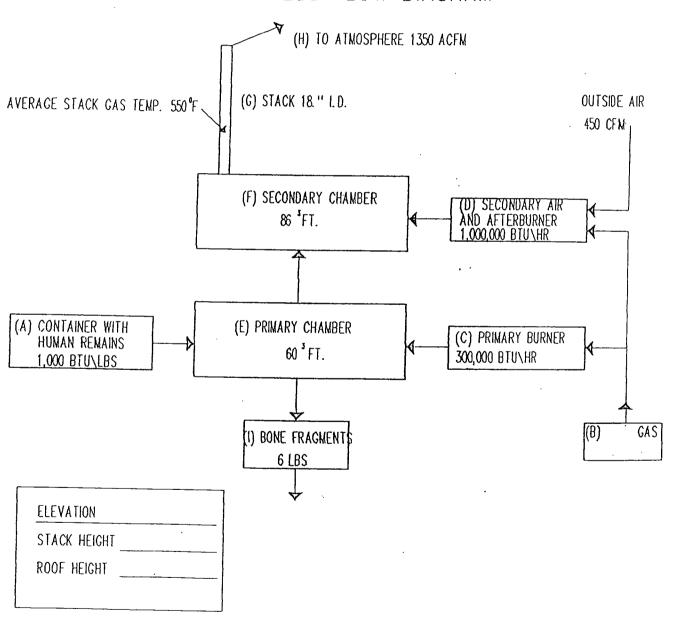
A type "K" thermocouple is placed 19³ ft. down stream of the flame tip to measure temperature, the signal is sent to the main control panel where it is received by a FUJI PYZ series temperature controller with digital readout and a DR4200 temperature recorder. The FUJI PYZ series temperature controller controls the temperature via a motorized butterfly valve located on the afterburner inlet gas assembly. Gas demand is controlled by temperature to maintain a steady temperature. The ignition/cremation burner is interlocked to the afterburning temperature by the FUJI PYZ series temperature controller set point. Combustion cannot start until temperature set point is reached. Alarm contacts in the FUJI PYZ series temperature controller are utilized for over (high) temperature conditions. 100° F over set point the afterburner will be in maximum low fire and the ignition/cremation burner will shut off. The butterfly valve located on the secondary air inlet is controlled by a separate temperature out put to add air to cool the system. At set point the unit will return to normal operation. An optimonitor smoke detector is placed on the stack and set at 10% opacity if emissions occur the alarm will sound; a visual red warning lamp located on the control panel will illuminate and the primary burners will shut off. The excess air butterfly valve will open to add air to the secondary chamber to oxidize the emissions. After a five (5) minute period the unit will revert to normal operation.



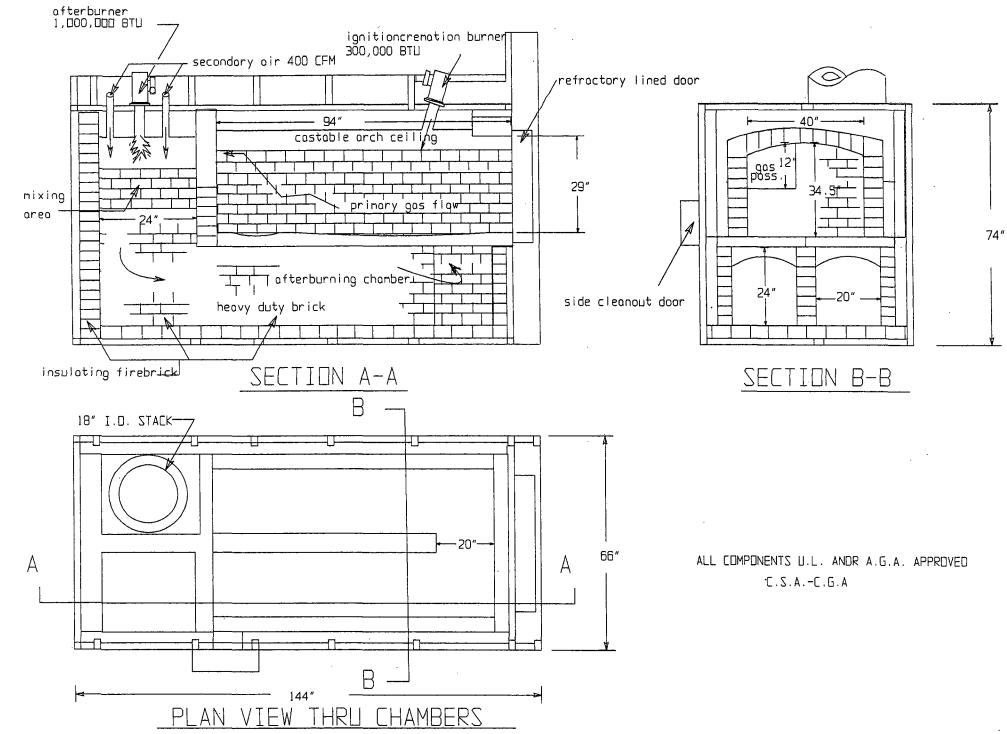
Systems, Inc.

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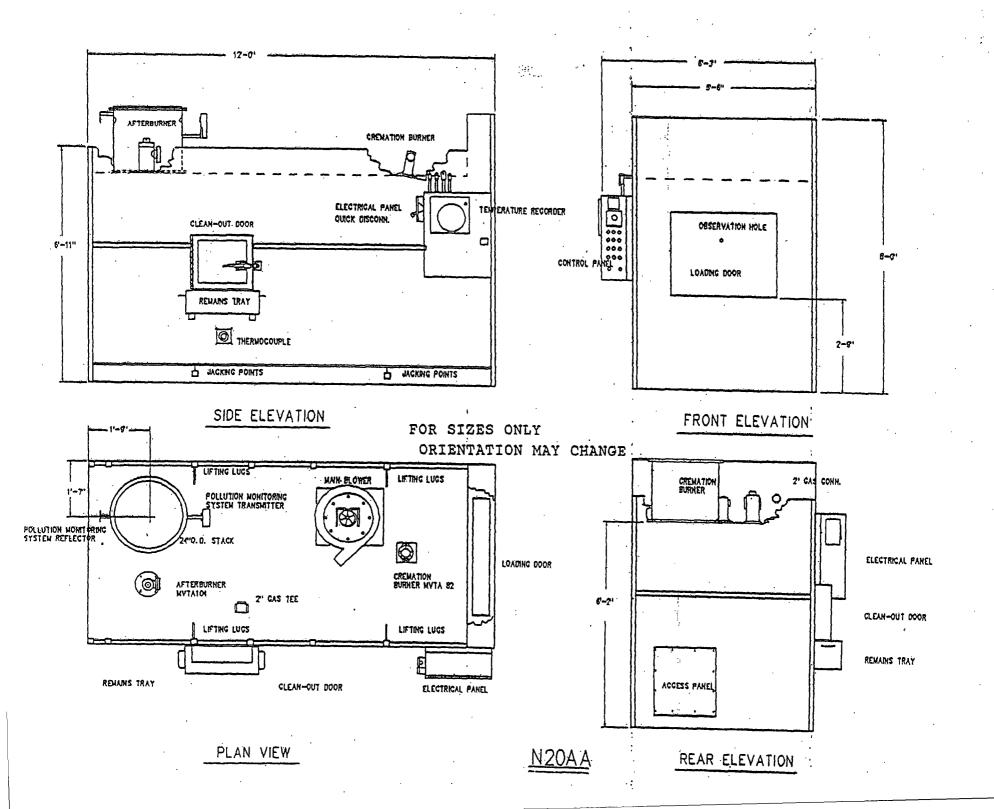
PROCESS FLOW DIAGRAM



World's Largest Independent Cremation Equipment Manufacturer



N20AA REFRACTORY



12/02/96

AFTERBURNER-

7178 P

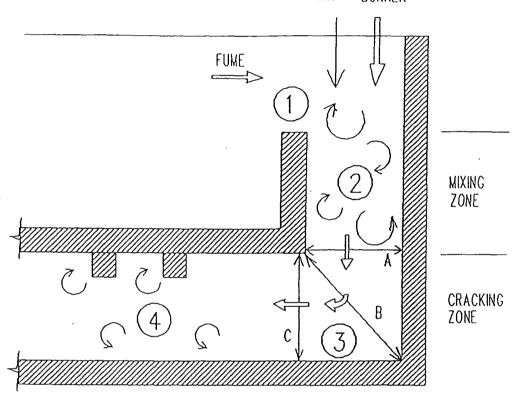


Systemiles, Inc.

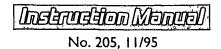
7205 - 114th Avenue North • Largo, Florida 33773 1-800-622-5411 • 727-541-4666 • Facsimile 727-547-0669

SECONDARY

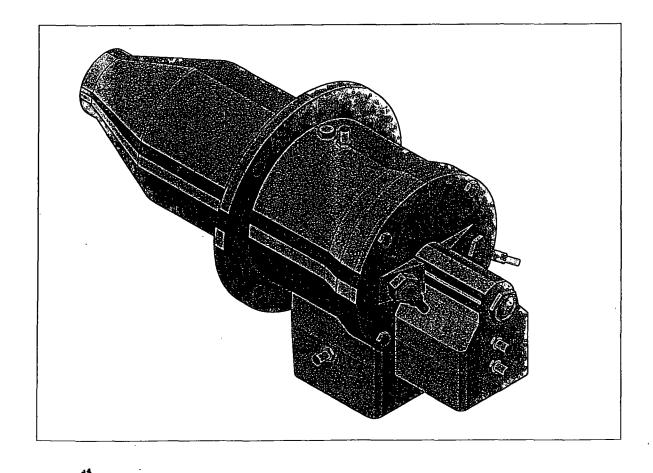
AIR BURNER



- 1. At the back of primary chamber, waste fume, air and burner flame all meet with different viscosities, volumes, velocities and flow directions which causes turbulence in the mixing zone of the secondary chamber.
- 2. Turbulence continues in the mixing zone as flows are traversing the flame tip.
- 3. Changing velocity at flame front zone and cornering cause additional turbulence at the base of the unit. $V_A > V_B < V_C$.
- 4. Uneven cross sectional area due to arches in the ceiling to support the primary chamber floor and additional changes in directional flow causes further turbulence downstream in the secondary chamber.



Eclipse Velocity Burners ThermJet Series (version 1.0)





Eclipse Combustion





INTRODUCTION

This section gives a detailed overview of the burner specifications. It also lists several options that are available for the ThermJet.

Figure 3.1 The ThermJet burner

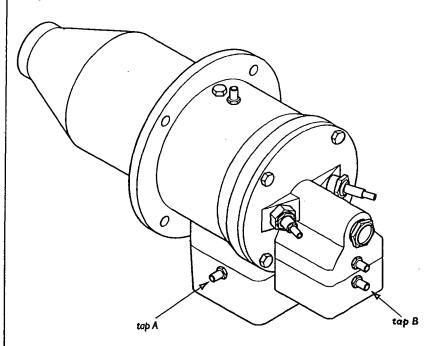


Table 3.1 Options

PARAVETER		OptiONS
Fuel	natural gaspropanebutane.	For any other mixed gas, contact Eclipse for orifice sizing.
Flame detection	U.V. scanner flame rod, for use with a	alloy or silicon carbide firing tubes only.
Ignition	direct spark ignition (6 l	kVAC).
Combustor	 alloy firing tube silicon carbide firing tub refractory block.	oe



SPECIFICATIONS

Main specifications

Thermjet performance data Table 3.2

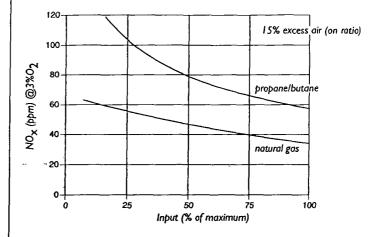
PARAMETER	BURNER	PROPERTY AND 18 A 1959		BURNI	RSEAR :	
	(VELOGI	T/)	30	165	1000	150
High fire input (Btu/hr)	Medium & High velocity		500,000	750,000	.1,000,00 0	1,500,00 0
Low firing rate, on-ratio (Btu/hr)	Medium & High ve	elocity	50,000	75,000	100,000	150,000
Low firing rate, fixed air (Btu/hr)	Medium & High ve	elocity	10,000	15,000	20,000	30,000
Static air pressure ("w.c.)	High velocity		12.0	16.0	14.5	18.5
 15% excess air, at maximum input with standard orifice plate installed, measured at tap A (See Figure 3.1) 	Medium velocity		7.5	8.0	7.5	9.5
Static gas pressure ("w.c.)	High velocity		11.0	15.5	16.0	16.5
 at maximum input with standard orifice plate installed. measured at tap B (See Figure 3.1) 	Medium velocity		6.0	6.5	7.5	8.0
Flame length (In)	High velocity	Nat. gas	25	30.4	33	38
(from end of firing tube)		Propane	33	34	34	42
		Butane	30	30	35	43
	Medium velocity	Nat. gas	28	28	38	43
		Propane	36	38	37	42
	Butane		39	30	42	40
Maximum flame velocity (ft/s)	High velocity		500	500	500	500
• 15% excess air, at maximum input	Medium velocity		250	250	250	250

- all information is given for general sizing purposes only refer to data sheet for burner specific information
- all inputs based on gross calorific values

Performance graphs

The graphs that follow give you an approximate picture of the performance. Should you want more exact information, contact Eclipse Combustion.

Figure 3.2 NO_x emissions

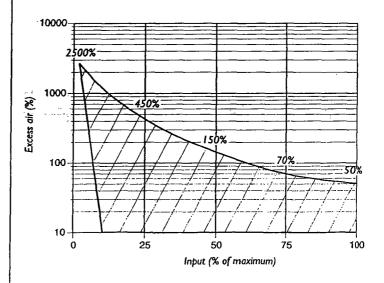


The emissions from the burner are influenced by:

- · the fuel type
- the combustion air temperature
- · the firing rate
- the chamber conditions
- the percent of excess air.

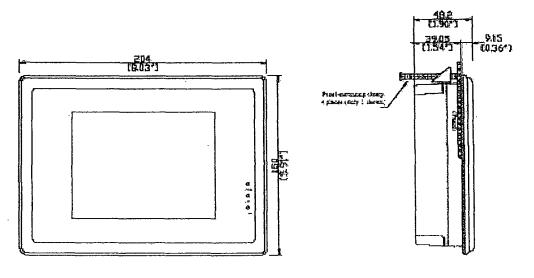
For estimates of other emissions, contact Eclipse Combustion.

Figure 3.3 Operational zone





Orion Drawings:

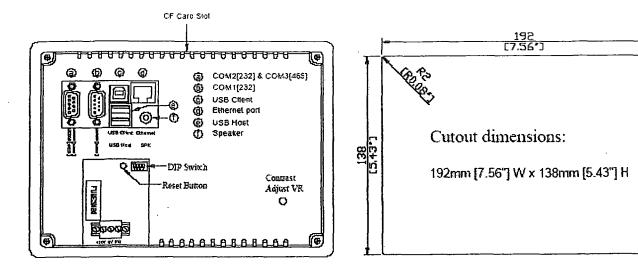


From View

Side View



Bottom View



Rear View



P.O Box 1196 * 7524 BridgeView, ILL 60455 * Phone: 888.751.5444 - Fax 888.245.2883

Power

24VDC - 500mA maximum current draw.

Display:

Display Type: STN Color LCD

Display Size: 5.7 O Max Colors: 4096 Resolution: 320 X 240

Pixel pitch (HxV,mm): 0.36 X 0.36

Luminance(cd/m2): 100 Storage Temp (C): -20 to 60 Operating Temp (C): 0 to 45

Backlight: 1 CCFL Contrast Ration: 30:1

Backlight life: Approx 40,000 hours

TouchScreen:

Type: 4 wire, analog resistive Resolution: Continuous

Light transmission: above 80% Life: 1 million activation minimal

Processor:

Type: Intel Xscale PXA255 200Mhz

Memory and OS:

Memory: 64MB of internal RAM Operating System: Windows CE.net

Loop Interface:

Type: 300 series control/RS485 multi-drop interface

Max Loops: 20

Data Storage:

Type: 128 Mb compact flash

Connections:

Serial: Com1, 2 & 3 - RS232/RS485

Ethernet: 10 baseT USB: 1 client - 2 host Sound: 16 bit sound output

Physical:

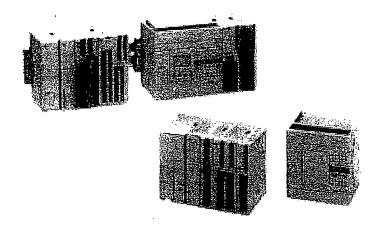
Front Panel: Meets Nema4/IP65

Shock: 10 to 25Hz (X,Y,Z direction 2G, 30 mins) Dimensions: 204Ó (H) x 150Ó (W) x 48Ó (D) - mm

Weight: 28.21.0 oz. (0.8 kg)

Orion interface ports (RS485, USB and Ethernet)

MicroSmart





UL Listed File No. E211795



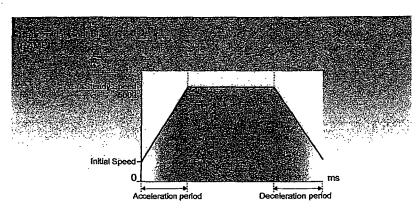
Pulse Output/Trapezoidal Control

Independent dual-axis control is available with two pulse outputs. Locational values can be easily defined for precise positional (trapezoidal) control.

- · Pulse output instruction
- PWM instruction (Pulse Width Modulation control)

Pulse Output Function Specifications

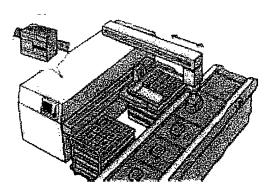
Number of output points	2
Maximum output frequency	20 kHz
*Only one point of transzoidal co	ontrol is available.



The Next Generation of PLC

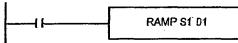
Key features of the MicroSmart series include:

- 10, 16, or 24 I/O All-in-one type CPU modules with Sink/ Source DC input and Relay Output
- 20 I/O Slim type CPU modules with Sink/Source DC input and Transistor Sink or Source Output
- 20 I/O Slim type CPU modules with Sink/Source DC input and Relay Output with high-speed Transistor Sink or Source Output
- 40 I/O Slim type CPU modules with Sink/Source DC input and Transistor Sink or Source Output
- DC Input, Relay Output, Transistor Output, Combination 1/0 and Analog I/O expansion modules available
- 24 I/O All-in-one CPU expandable to 88 I/O points; 20 I/O slim types expandable up to 148 or 244 I/O; 40 I/O slim type expandable up to 264 I/O points
- Standard RS232 port, optional plug-in RS485/RS232 port
- · Optional memory cartridge or real-time clock and calendar cartridge
- Data link to other MicroSmart modules, PLCs, PCs or HG series operator interfaces
- Approved for Class 1—Div. 2 hazardous locations (UL1604)
- · Compact size
- · Now available with AC input expansion module



Setting the desired values enables you to precisely manage the trapezoidal control

1
50
10
2
10,000



Programmable Logic Controllers

Programmable Logic Controllers



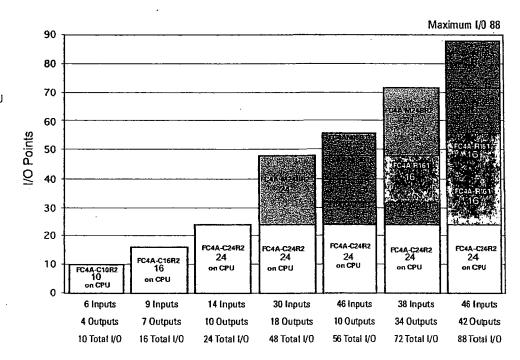
Calquast Individua @ Combinetion (Company)

All-In-One Type

- Attach Maximum 4 Expansion Modules
- Maximum I/O 88 points
- Only FC4A-C24R2/C24R2C CPU Module is expandable



The maximum number of relay outputs that can be turned on simultaneously is 33 points including relay outputs on the CPU module.



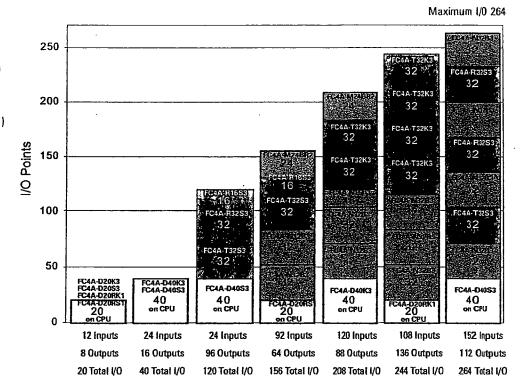
Slim Type



- Attach Maximum 7 Expansion Modules
- Maximum I/O
- 148 points (D20K3, D20S3)
- 244 points (D20RK1, D20RS1)
- -264 points (D40K3, D40S3)

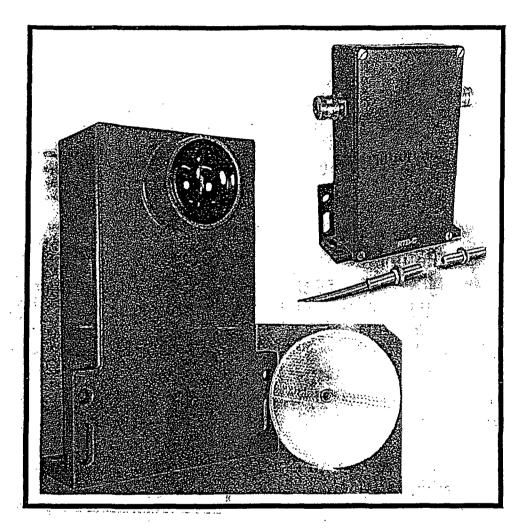


The maximum number of relay outputs that can be turned on simultaneously is 54 points including relay outputs on the CPU module.





VISIBLE EMISSIONS ALARM (VEA)



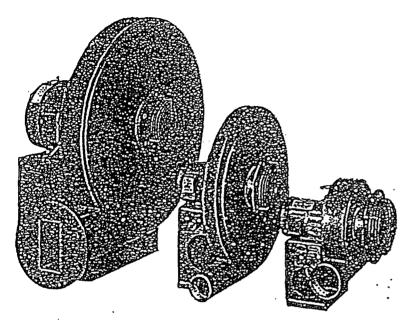
APPLICATION: Alarm and control for **Opacity** used on small and large sources for warning operators and shutting down systems based on opacity, haze or clarity.

- Proven Rugged Design
- Unaffected by Ambient Light
- Spans up to 6 Feet
- Visible LED Light Source

- Dual Beam or Single Beam
- Adjustable Delay up to 3 min.
- Easy to Install & Support
- External Adjustment

ECLIPSE TURBO BLOWERS

SERIES "SMJ"



- · High efficiency
- · Heavy gauge steel base and housing
- Aluminum impellers balanced statically and dynamically
- Matching air filters available
- Changeable outlet positions

Eclipse "SMJ". Blowers are centrifugal blowers that provide low pressure air for industrial combustion systems. They are also used for cooling, conveying, drying, liquid agitation, smoke abatement, vacuum cleaning, fume and dust exhausting, and other plications where air temperatures are under 220°F.

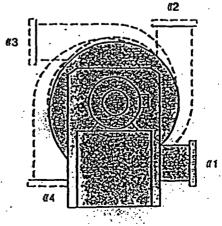
All "SMJ" Blowers are constructed of continuous welded, heavy gauge steel. The impellers are made of lightweight high strength, riveted aluminum. Outlets on 3" and 4" models are threaded, while all others are flanged for a standard 125# ANSI companion flange. Discharge ports are sized to keep pressure losses within reasonable limits.

Blower inlet flanges are equipped with a grill that complies with OSHA regulations. If desired, the grill may be removed and the inlet bolted to a standard ANSI companion flange. Eclipse-supplied motors are standard shaft and starting torque, ball bearing, 3600 rpm units. On any blower requiring 3/4 HP or more, Eclipse recommends that polyphase motors be used.

There are four possible outlet positions. Any existing position is easily changed by removing the housing from the

blower base and remounting it in the desired position. Positions 1 through 3 can be specified for any blower. Position 4, however, requires factory approval before ordering. Position 1 is the standard assembly (bottom, horizontal) unless otherwise specified.

"SMI". Blowers can be supplied with counterclockwise (CCW) or clockwise (CW) rotation as viewed from the motor side. CCW rotation is furnished standard unless otherwise specified.



Outlet Positions

Table 5.5-5
ELEMENTAL CONTENT OF BODY FAT AND
BODY WATER

Component	Mass (g)	Carbon Quantity* (g)	Hydrogen Quantity* (g)	Oxygen Quantity (g)
Body fat	13,500	1.0E + 4	1.6E + 3	1.5E + 3
Essential	1,500	1.2E + 3	1.8E + 2	1.7E + 2
Nonessential	12,000	9.2E + 3	1.4E + 3	1.3E + 3
Body water	42,000		4.6E + 3	3.7E + 4
Extracellular	18,000		20.E + 3	1.6E + 4
Intracellular	24,000	•	2.6E + 3	2.1E + 4

· For sources, see Reference 1.

From Snyder, W. S., Cook, M. J., Karhausen, L. R., Nasset, E. S., Howells, G. P., and Tipton, I. H., Report of the Task Force on Reference Man. ICRP Report No. 23, International Commission on Radiological Protection, Pergamon Press, Oxford, 1975, 1. With permission.

Table 5.5-6
REFERENCE MAN: TOTAL BODY CONTENT FOR SOME ELEMENTS

		Percent of total body			Percent of total body
Element	Amount (g)	weight	Element	Amount (g)	weight
Oxygen	43,000	61	Lead	0.12	0.00017
Carbon	16,000	23	Соррег	0.072	0.00010
Hydrogen	7,000	10	Aluminum	0.061	0.00009
Nitrogen	1,800	2.6	Cadmium	0.050	0.00007
Calcium	1,000	1.4	Boron	<0.048	0.00007
Phosphorus	780	1.1	Barium .	0.022	0.00003
Sulfur	140	0.20	Tin ·	< 0.017	0.00002
Potassium	140	0.20	Manganese	0.012	0.00002
Sodium	100	0.14	lodine	0.013	0.00002
Chlorine-	. 95	0.12	Nickel	0.010	0.00001
Magnesium	19	0.027	Gold	<0.010	0.00001
Silcon	18	0.026	Molybdenum	<0.0093	0.00001
Iron	4.2	0,006	Chromium	<0.0018	0.000003
- Fluorine	2.6	0.0037	Cesium	0.0015	0.000002
Zinc	2.3	0.0033	Cobalt	0.0015	0.000002
Rubidium	0.32	0.00046	Uranium	0.00009	0.0000001
Strontium	0.32	0.00046	Berylium	0.000036	
Bromine	0.20	0.00029	Radium	3.1 × 10-"	•

From Snyder, W. S., Cook, M. J., Karhausen, L. R., Nasset, E. S., Howells, G. P., and Tipton, I. H. Report of the Task Group on Reference Man, ICRP Report No. 23, International Commission on Radiological Protection, Pergamon Press, Oxford, 1975, I. With permission.

EMISSIONS TESTING of the FIRST CALL CREMATORY B & L CREMATION SYSTEMS, INC. N20 SERIES HUMAN CREMATORY Clearwater, Florida

April 5, 2008

FDEP Permit No. 1030473-008AG EU No. 008 SES Reference No. 08S131

Conducted by:

SOUTHERN ENVIRONMENTAL SCIENCES, INC. 1204 North Wheeler Street Plant City, Florida 33566 Phone (831) 752-5014, Fax (813)752-2475

Project Participants

Byron E. Nelson Mark S. Gierke Dale A. Wingler Travis B. Nelson

SPECIAL EMISSIONS

EMISSION TESTING

of the

FIRST CALL CREMATORY B & L CREMATION SYSTEMS, INC. N20 SERIES HUMAN CREMATORY Clearwater, Florida

April 5, 2008

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1.0 INTRODUCTION

Southern Environmental Sciences, Inc. conducted emissions testing of the First Call Crematory, B & L Cremation Systems, Inc. N20 Series human crematory on April 5, 2008. This facility is located at 12660 34th Street North, Clearwater, Florida. Testing was conducted for particulates, carbon monoxide (CO), sulfur dioxide (SO₂), nitrogen oxides (NOx), total hydrocarbons (VOC) and visible emissions. Oxygen (O₂) concentrations were measured to correct emission rates to 7% O₂. Mr. Jose Rodriguez of the Pinellas County Department of Environmental Management was present as an observer during a portion of the testing.

2.0 SUMMARY OF RESULTS

Results of the particulate, carbon monoxide, sulfur dioxide, nitrogen oxides and total hydrocarbons are summarized in Table 1. A visible emissions evaluation was performed over a one hour period. The average maximum six minute opacity was zero percent.

3.0 PROCESS DESCRIPTION

The B & L Cremation Systems N20 Series crematory incinerator cremates human remains in an environmentally acceptable manner. The unit consists of a primary and secondary (afterburner) chamber each fired with natural gas. The unit is designed to incinerate human remains at a rate of 150 pounds per hour with a maximum heat input rate of 1.5 MMBTU per hour (primary chamber 0.5 MMBTU per hour, secondary chamber 1.0 MMBTU per hour).

TABLE 1. EMISSIONS TEST SUMMARY

Company: FIRST CALL CREMATORY

Source: B & L Cremation Systems, Inc.

N20 Series Human Crematory

	Run 1	Run 2	Run 3
Date of Run	4/5/08	4/5/08	4/5/08
Weight of Human Remains (lbs.)	170	165	140
Start Time (24-hr. clock)	1005	1348	1722
End Time (24-hr. clock)	1107	1452	1824
Vol. Dry Gas Sampled Meter Cond. (DCF)	39.324	47.848	41.832
Gas Meter Calibration Factor	0.994	0.994	0.994
Barometric Pressure at Barom. (in. Hg.)	30.39	30.29	30.39
Elev. Diff. Manom. To Barom. (ft.)	0	0	0
Vol. Liquid Collected Std. Cond. (SCF)	3.305	5.073	2.966
Moisture in Stack Gas (% Vol.)	7.8	9.9	8.6
Molecular Weight Wet Stack Gas	28.48	28.17	28.62
Stack Gas Static Press. (in. H2O gauge)	-0.03	-0.03	-0.03
Average Square Root Velocity Head	0.166	0.208	0.187
Average Orifice Differential (in. H2O)	1.132	1.669	1.291
Average Gas Meter Temperature (°F)	81.5	88.3	91.7
Average Stack Gas Temperature (°F)	834.3	1013.6	998.3
Pilot Tube Coefficient	0.84	0.84	0.84
Stack Gas Vel. Stack Cond. (ft./sec.)	16.78	19.88	17.65
Effective Stack Area (sq. ft.)	1.87	1.87	1.87
Stack Gas Flow Rate Std. Cond. (DSCFM)	623	715	659
Stack Gas Flow Rate Stack Cond. (ACFM)	1,833	2,202	1,977
Net Time of Run (min.)	60	60	60
Nozzle Diameter (in.)	0.600	0.600	0.600
Percent Isokinetic	98.7	102.6	97.6

TABLE 1. EMISSIONS TEST SUMMARY (con't)

Company: FIRST CALL CREMATORY

Source: B&L Cremation Systems, Inc.

N20 Series Human Crematory

	Run 1	Run 2	Run 3	;
Date of Run	4/5/08	4/5/08	4/5/08	
Weight of Human Remains (lbs.)	170	165	140	
Start Time (24 hr. clock)	1005	1348	1722	
End Time (24 hr. clock)	1107	1452	1824	
Oxygen (%)	12.7	12.1	13.1	
Particulate Collected (mg.)	27.0	69.1	99.2	
•				(Avg.)
Particulate Emissions (gr./DSCF)	0.011	0.023	0.038	0.024
Particulate Emissions (gr./DSCF @ 7% O2)	0.018	0.036	0.066	0.040
Particulate Emissions (lb./hr.)	0.06	0.14	0.21	0.136
CO Emissions (ppm)	3.05	2.27	4.98	3.43
CO Emissions (ppm @ 7% O2)	3.4	2.95	6.7	4.35
CO Emissions (lb./hr.)	0.007	0.006	0.018	0.010
NOx Emissions (ppm)	110.23	122.3	115.7	116.1
NOx Emissions (lb./hr.)	0.58	0.71	0.74	0.677
VOC Emissions (ppm)	1.5	0.80	1.41	1.237
VOC Emissions (lb./hr.)	0.007	0.004	0.009	0.007
SO ₂ Collected (mg)	33.1	49.4	59.7	47.4
· •	0.088	0.142	0.167	0.13

Note: Standard conditions 68°F, 29.92 in. Hg

1.0 MMBTU/hr.). Emissions are controlled by the afterburner that is preheated and maintained at a minimum operating temperature of 1600°F prior to and during ignition of the primary chamber. Process operational data was provided by facility personnel and is included in the appendix.

4.0 SAMPLING PROCEDURES

4.1 Methods

All sampling was performed using methods currently acceptable to the FDEP. All test methods are contained in Title 40 of the Code of Federal Regulations, Appendix A and are as follows:

Pollutant	EPA Method No.	<u>Title</u>
Particulates	5	Determination of Particulate Emissions from Stationary Sources
Carbon Monoxide	10	Determination of Carbon Monoxide Emissions from Stationary Sources
Oxygen	3B	Gas analysis for the Determination of Emissions Rate Correction Factor or Excess Air
Nitrogen Oxides	7E	Determination of Nitrogen Oxides Emissions from Stationary Sources (Instrumental Analyzer Procedure)
Sulfur Dioxide	6	Determination of Sulfur Dioxide Emissions from Stationary Sources, Section 2.1
Total Hydrocarbons	25A	Determination of Total Gaseous Organic Concentration Using a Flame Ionization Analyzer
Visible Emissions	9	Visual Determination of the Opacity of Emissions of Stationary Sources.

Sulfur dioxide emissions were determined simultaneous with particulates as per Section 6.1 of EPA Method 6.

4.2 Sampling Locations

Locations of the sample ports and stack dimensions are shown in Figure 1.

Particuale/SO₂ sampling was accomplished by conducting horizontal traverses through each of two ports located on the stack at a ninety degree angle from one another. Twenty four sample points were chosen in accordance with EPA Method 1 – Sample and Velocity Traverses for Stationary Sources, 40 CFR 60, Appendix A. Carbon monoxide, nitrogen oxides, total hydrocarbon and oxygen sampling were performed from the same

4.3 Sampling Trains

sampling ports as the particulate/SO₂ sampling.

The particulate/SO2 sampling train consisted of a 3 foot Inconnel probe utilizing a one piece quartz glass nozzle and liner, a heated glass fiber filter and four impinges arranged as shown in Figure 2. Flexible tubing was used between the heated filter and the impingers. The first impinger was charged with 100 milliliters of 80% isopropanol, the second and third impingers were each charged with 100 milliliters of a 3% percent hydrogen peroxide solution and the fourth impinger was charged with indicating silica gel desiccant. The impingers were cooled in an ice and water bath during sampling. A Nutech Corporation control console was used to monitor the gas flow rates and stack conditions during sampling.

The carbon monoxide sampling train consisted of a stainless steel probe, Teflon sample line, condenser, silica gel and carbon dioxide adsorbent tubes and a Thermo Environmental Instruments, Inc. Model 48 Gas Filter Correlation CO analyzer arranged as shown in Figure 3.

The nitrogen oxides sampling train consisted of a stainless steel probe, Teflon sample line, and a California Analytical Inc. Model 300 FID analyzer arranged as shown in Figure 5.

The oxygen sampling train consisted of a probe, sample line, tedlar bag in a rigid container, valve, vacuum pump, and flow meter.

4.4 Sample Collection

Prior to particulate/SO₂ sampling, the pitot tubes were checked for leaks and the manometers were zeroed. A pretest leak check of the sampling train was conducted by sealing the nozzle and applying a 15" Hg vacuum. A leak rate of less than 0.02 cubic feet per minute was considered acceptable. Sample was collected isokinetically for two and one half minutes at each of the points sampled.

All instrumental analyzers were calibrated immediately prior to the beginning and checked after each run by introducing known gases into the instrument through the sampling.

The tedlar bag used for obtaining an integrated oxygen sample was leak checked prior to the test by pressurizing it to 2 to 4 in. H₂O and allowing it to stand overnight. The bag was considered leak free if it remained inflated. A one hour integrated sample was obtained at a rate 0.5 liters per minute for each run.

All sampling was conducted simultaneously.

4.5 Sample Recovery

A post test leak check of the particulate/SO2 sampling train was performed at the completion of each run by sealing the nozzle and applying a vacuum equal to or greater than the maximum valve reached during the sample period. A leak rate of less than 0.02 CFM or 4 percent of the average sampling rate (whichever was less) was considered acceptable. The probe was then disconnected, the ice bath was drained and the remaining part of the sampling train was purged by drawing charcoal filtered air through the system for fifteen minutes at the average flow rate used during sampling. The nozzle and probe were then brushed and rinsed with reagent grade acetone and the washings were placed in clean polyethylene containers and sealed. The glass fiber filter was removed from the holder with forceps and placed in a covered Petri dish for return to the laboratory. The front half of the filter holder was rinsed with acetone and the washings were added to the nozzle and probe wash. The contents of impingers 1 through 3 were measured volumetrically and the silica gel in the fourth impinger was weighed to the nearest 0.1 gram for determination of moisture content. The 80 percent isopropanol in the first

impinger was discarded and the impinger was rinsed with demonized, distilled water. The 3 percent hydrogen peroxide in the second and third imingers was placed in a clean polyethylene sample bottle. The imingers, associated glassware and back half of the filter holder were then rinsed with de-ionized, distilled water which was added to the sample bottle.

Two calculations of the moisture content of the stack gas were made for each run, one from the impinger analysis and one from the assumption of saturated conditions based upon the average stack gas temperature and a psychrometric chart as described in EPA Method 4, Determination of Moisture Content in Stack Gases, 40 CFR 60, Appendix A. The lower of the two values of moisture content was considered to be correct and was used in the emissions computations.

5.0 ANALYTICAL PROCDURE

5.1 Pretest Preparation

The glass fiber filters for the particulate train were numbered, oven dried at 105°C for two to three hours, desiccated and weighed to a constant weight in preparation for the test. Results were recorded to the nearest 0.1 milligram. Filters were loaded into holders and a filter was set aside as a control blank. The imingers were charged as described in section 4.3 and the contents of the fourth impinger were weighed to the nearest 0.1 gram. The 3 percent hydrogen peroxide solution for the sulfur dioxide sampling was prepared the morning of the test from 30 percent reagent grade stock solution.

5.2 Analysis

Upon return to the laboratory, the particulate filters were removed from the containers with forceps, dried at 105°C for two to three hours, desiccated and weighed to a constant weight. Results were recorded to the nearest 0.1 milligram. The probe and nozzle washes and an acetone blank were measured volumetrically and transferred to clean, tared evaporating dishes and evaporated to dryness over low heat. The evaporating dishes were then oven dried at 105°C for two to three hours, desiccated and weighed to a constant weigh. Results were recorded to the nearest 0.1 milligram. The total particulate reported is the sum of the filter weight gain and the weight gain of the evaporating dishes, corrected for the acetone blank. The impinger solutions were analyzed for sulfur dioxide procedures specified in Section 4.3 of EPA Method 8.

PROJECT PARTICIPANTS AND CERTIFICATION

FIRST CALL CREMATORY B & L CREMATION SYSTEMS, INC. N20 SERIES HUMAN CREMATORY Clearwater, Florida

April 5, 2008

Project Participants:

Marke S. Gierke Byron E. Nelson Dale A. Wingler Travis B. Nelson

Kenneth M. Roberts

Certification:

I certify that to my knowledge all data submitted in this report is true and correct.

Southern Environmental Sciences, Inc. 1204 North Wheeler Street | Plant City, Florida 33563 | (813) 752-5014, Fax (813) 752-2475

VISIBLE EMISSIONS EVALUATION

COMPANY FIRST Cal	1 Crimatory					
UNIT NOO AA Ciemalory Incinerator						
ADDRESS 12660 34 th Si. N # A-1						
Clearwater						
PERMIT NO.	COMPLIANCE?					
1030473-003-176 AIRS NO. 1032477	5000					
PROCESS RATE	PERMITTED RATE Advir 5176 8:47 - (150 15) hr					
PROCESS FOUIPMENT	imatory Faciliariator					
CONTROL EQUIPMENT	busner					
OPERATING MODE . MIT. GS FIVE A	AMBIENT TEMP. (° F) START \$5 STOP \$5					
HEIGHT ABOVE GROUND LEVEL START 130' STOP DEMINE	HEIGHT RELATIVE TO OBSERVER START 130' STOP Jone					
DISTANCE FROM OBSERVER START U90' STOP . Juml	DIRECTION FROM OBSERVER COSTART 500 STOP 50					
EMISSION COLOR	PLUME TYPE NA A CONTIN. C INTERMITTENT C					
WATER OROPLETS PRESENT?	IS WATER DROPLET PLUME W/17					
POINT IN PLUME AT WHICH OPACITY I	WAS DETERMINED STOP SAME					
DESCRIBE BACKGROUND START SKY	STOP SKY					
BACKGROUND COLOR STARTBIJULT STOP DOTTE	SKY CONDITIONS, START SCATTER STOP DAME					
WIND SPEED (MPH) START 0-10 STOP DOWNE	WIND DIRECTION STARTVALL STOP VAL.					
AVERAGE OPACITY FOR O O	RANGE OF OPACITY READINGS MIN. MAX.					
SOURCE LAYOUT SKETCH	Draw North Arrow					
·	Emission Point					
·						
* Wind	Observer's Position					
Sun	140 All Location Acta					
Comments						

OBSERVAT	====	E		START TI	ме 48		STOP TI		
SEC					SEC				
MIN	O	15	30	45	MIN	0	15	30	45
0	0	0	0	0	30	0	0	0	0
1	12	0	0	0	31	0	0	0	0
2	0	0	0	0	32	0	0	0	0
3	0	0	0	0	33	0	0	0	0
4	0	0	0	0	34	0	0	0	0
5	0	0	0	0	35	12	0	0	0
6	D	0	0	0	36	0	0	0	0
7	0	0	0	0	37	0	0	0	0
8	0	0	0	0	38	12	0	0	0
9	0	0	0	0	39	0	0	0	0
10	0	(2)	0	0	40	0	0	0	121
11	0	\mathcal{O}	Õ	0	41	0	0	0	0
12	0	0	0	0	42	0	0	0	2
13	(2)	Q	0	0	43	0	0	0	0
14	12	Q	0	0	44	0	0	0	0
15	0	0	0	0	45	0	0	0	0
16.	0	0	0	0	46	0	0	0	0
17	0	0	0	0	47	0	0	0	0
18	Q	0	0	0	48	0	0	0	0
19	0	0	0	10	49	0	0	0	0
20	0	0	0	0	50	0	0	0	0
21	0	0	0	0	51	0	0	0	0
22	\mathcal{D}	0	0	0	52	0	0	0	00
23	0	0	0	0	53	0	0	0	0
24	0	0	0	0	54	0	0	0	0
25	0	0	0	0	55	0	0	0	0
26	0	0	0	Q	56	0	0	Q	0
_27	0	0	0	0	57	0	0	0	0
28	0	0	0	0	58	0	0	0	\bigcirc
29	<u> 0</u>	\bigcirc	0	0	59	0	0	0	0
OBSERV	ER: //	la it	(Gi.	ick.					
Certified		11.0	,			Certifie	ed at:	Tanpa.	FL
Date Cer	rtified:	2/0	8	Exp.	Date:	81	08		
I certify was true	that all	data p	rovide			on con	ductin	g the t	est
Signatur	e: 🍾	lee f	roc	233	<u>- WT</u>	<u>. s</u>	Taile	menI	-
Title:									

Process Weight Statement

DATE 4 5 08	SAMPLING TIME: FROM <u>'10,05</u> A.I	М. ТО <u>ь 24</u> Р.М.
STATEMENT OF PRO	CESS WEIGHT	r
COMPANY	FIRST CAL CREMAT	7.R.Y.
	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	
MAILING ADDRESS	12660 3471 ST. N. CEGARL	LATER FL
SOURCE IDENTIFICATION	B&L Systoms N.20:	
SOURCE LOCATION	12660 34th ST. N. CLAGA	
DATA ON OPERATING	· · · · · · · · · · · · · · · · · · ·	
START OF OPERATION TIME	1	
END OF OPERATION, TIME		
ELAPSED TIME		
IDLE TIME DURING CYCL	E	
DESIGN PROCESS RATING	PROCESS WEIGHT RATE (INPUT)	150 lb/R1
	PRODUCT (OUTPUT)	
DATA ON ACTUAL PR	OCESS RATE DURING OPERATION	RATE 160 bs (Bun)
MATERIAL	i	RATE 155 lbs (Run 2
MATERIAL	i. ii	RATE 140 bs (Runs)
AVERAGE PROCESS WEIGHT		RATE
PRODUCT		RATE
PRODUCT		RATE
PRODUCT		RATE
I certify	that the above information is true and correct to	o the best of my knowledge. Name (Please Print)
	Signature	
	Title OXia	ata.

PARTICULATE MATTER COLLECTED

PARTIC	ULATE MA	ATTER COLI	ECTED		
PLANT: FIRST CALL CRG	MITGE	1.			
UNIT NO.: B & L CREMATION S			ERIES HUMA	N CREMATORY	
TEST DATE: 4/5/08					
1301 21112. 113100		ANALYZ	ED BY:	MG	
Acetone blank container no.	405		Filter blank	по. 6752	•
Acetone blank volume, ml., (VA)	200		Filter blank	tare weight, g. 0.3402	
Acetone blank final weight, g.	101.0509		Filter blank	final weight, g. 0.3409	
Acetone blank tare weight, g.	101.0507		Filter weigh	nt diff., g. 0.0007	
Acetone blank weight diff., g. (ma)	0.00012				
Run No.	1	Container Number	Weight of F		
			Final Weight	Tare Weight	Weight Gain
Filter No.	6768	1 (Filter)	0.3603	0.3434	0.0169
Liquid lost during transport	0	2 (Wash)	103.1076	105.6522	0.0102
Acetone wash volume, ml (Vaw)	100			Total ⁻	0.0271
Acetone wash reside, g.(Wa)	0.0001	}		Less acetone blank, g. (Wa)	0.0001
Acetone wash container no.	4	300	Weight of particulate matter, g		
Run No.	2				
Filter No.	6770	Container	Maight of D	Indiaulata Callagtad	
Liquid lost during transport, ml.	0	Number	Final	articulate Collected	Weight
Acetone wash container no.	18		Weight	Tare Weight	Gain
Acetone wash volume, ml (Vaw)	125	1 (Filter)	0.3972	0.3391	0.0581
Acetone wash reside, g.(Wa)	0.0001	2 (Wash)	105.6633	105.6522	0.0111
				Total	0.0692
				Less acetone blank, g. (Wa)	0.0001
				Weight of particulate matter, g	0.0691
Run No.	3				
Filter No.	6769	Container Number	Weight of D	articulate Collected	
Liquid lost during transport, ml.	0	MULLIDEL	Final	articulate Collected ,	Weight
Acetone wash container no.	53	'	Weight	Tare Weight	Gain
Acetone wash volume, ml (Vaw)	130	1 (Filter)	0.4182	0.3373	0.0362
Acetone wash reside, g.(Wa)	0.0001	2 (Wash)	100.6350	100.6166	0.0184

Total

Less acetone blank, g. (Wa)

Weight of particulate matter, g

0.0993

0.0001

0.0992

MOISTURE COLLECTED

Plant	FIRST CON CROWN	tory.				
Unit Date Run N	NZOAA CREMTTON	,				
	Inpinger Number	1	2	3	4	Weighed by:
	Final Weight (g):	160:0	104.0	_0_	259.4	DW
	Initial Weight (g):	10 <u>0.0</u>	(<u>201</u> 0	0	253.3	DH
	Difference (g):	60.0	40	_0_	6.1	
	Total Condensate (g):				70.1	
Unit Date Run N	Cheractory 4/5/08 0. 2					. المحادة والمسترد والمرادية والمحادثة المحادة والمحادثة والمحادث والمحادثة والمحادثة والمحادثة والمحادثة
	Impinger Number	1	2	3	4	Weighed by:
	Final Weight (grams)	195.0	105.0	0_0	266.8	M
	Initial Weight (grams)	100.0	100.0	0	259.2	DN
	Difference (grams)				7.6	
	Total Condensate (grams)				107.6	
Unit Date Run #	Ulema Today 45 08.					·
	Impinger Number Final Weight Initial Weight (grams) Difference (grams) Total Condensate (grams)	•	1 44.0 100.0 44.0	2 110:0 10:0	0 0	4 Weighed by: 263.2 DW 543 DW 8.9 62.4

FIELD DATA SHEET

Company Fir	st Call Crea	natory	Run No.	
Source N20AA	Crenatory	-	Date 4/5/08	
Operator(s) MC/TN	10w !	24	hr. time at start 1005	
•	1	24	hr. time at end 1167	
Dimensions Dia	,1	Fi	Iter No(s) <u>C 768</u>	
LxW	18.5"	Ва	arometric Pressure ("Hg) <u>30,39</u>	
Static Press. ("H2O)	-0.03	Elev Diff. M	Iano. To Barom. (Ft.)	
Meter Box No.	_001	Ambient Te	mperature (F°)	
Meter ΔH@	1,450			
Meter Correction Factor	0.994	Assumptions		
Pitot Tube Cp	84	% Moisture <u>10</u>	Sample Train Leak Check:	
Nozzle ID		Stack Temp. 1000	Initial O, W5 CFM @ 15 "Hg	
Nozzle Dia. (Inches)	0.600	Meter Temp. <u>60</u>	Final <u>O. 007</u> CFM @ 15 "Hg	/
Probe Length/Liner	3 quartz	Md/Ms 1.04	Initial Pilot Tube (-) (+)	,
		K Factor 36.	Final Pitot Tube (-) (+)	_

Moist. Co	ollected: - In	np. No. I	,Imp.	No. 2 & 3	,Imp. No 4	,To	otal Filter	Tare Wt.		
Point #	Sample Time	Meter Vol. Vm	Vel. Head ΔP ("H2O)	Original Diff. AH ("H2O)	Stack Temp., Ts _(sF)	Meter Temp., Tm (•F)	Hot Box Temp (•F)	Exit Temp. (•F)	Pump Vacuum ("Hg)	Other
1	\circ	234,328	,03	1,10	787	GQ	246	63	3,5	<u> </u>
2	2,5	236.03	.63	1.10	796	69	249	63	-3.0	<u> </u>
3	S,o	23764	,035	1.30	810	70	248	62	3,0	
4	7.5	239,34	,03	1.10	796	70	245	GI	3.0	<u> </u>
5	10.0	240.96	,03	1.00	802	73	244	Go	3.0	1
6	12.5	242.56	,०३	1.40	806	75	240	58	3.0	<u> </u>
7	15.0	244.32	.03	1.40	808	77	241	_58	3.0	
88	17.5	246.14	,02	.94	785	79	239	57	2.0	1
9	20.0	247.70	.02	,94	777	40	239	56	2.0	
10_	22.5	249,21	.015	,58	783	<i>40</i>	237	56	115	
11	25,0	250,51	.02	.94	791	gl	235	55	2.0	<u></u>
12	27.5	252,19	,02	.94	790	82	238	54	2.0	
13	30,0	25350	.02	,94	405	82	243	53	2.5	
14	32.5	255,00	,02	X.94	832	8.4	249	53	2.0	
15	35,0	256.54	,025	1.15	840	85	242	53	2.5	
16_	37.5	258,17	,025	1,15	839	86	240	53	2.5	
17_	40.0	259.83	,025	1.15	843	8 Ç	239	52	2.5	
18	42.5	261.49	.025	1.15	851	87	235	53	2.5	
19	45,0	203.14	,03	1.35	899	88	234	53	3.0	
20	47.5	264,89	.035	1,30	905	90	233	52	3.0	
21		266.63	.03	1.35	912	90	233	52	3.0	
22		204.30	.03	1.35	918	au	235	52	3.5	
23	55.0	270.05	,03	1,35	921	91	238	51	3.0	
24	57.5	271.87	103	1.35	926	92	240	51	3.5	
	60.0	273,652		·····						

FIELD DATA SHEET

_			^
Company Fig	st Call Cro	enatory	Run No. 2
Source N20AA	Crematory		Date $\frac{4/5/03}{}$
Operator(s) TN/MG	/DW 1	24 hr. ti	me at start 13 '48
(24 hr. ti	me at end $14:52$
Dimensions Dia		Filter N	o(s). <u>6770</u>
LxW D	18,5"	Barome	tric Pressure ("Hg) 30,039
Static Press. ("H2O)	03	Elev Diff. Mano.	To Barom. (Ft.)
Meter Box No.	001	Ambient Tempera	uture (F°) <u>85</u>
Meter ΔH@	1,450		
Meter Correction Factor	0,944	Assumptions	
Pitot Tube Cp	, 84	% Moisture 10	Sample Train Leak Check:
Nozzle ID		Stack Temp. <u>900</u>	Initial 0.002 CFM @ 15 "Hg
Nozzle Dia. (Inches)	0.600	Meter Temp. <u>90</u>	Final <u>0.002</u> CFM @ 12 "Hg
Probe Length/Liner	3 Quarte	Md/Ms i.o4	Initial Pilot Tube (-) (+)
		K Factor 39.45	Final Pitot Tube (-)(+)

Moist. C	ollected: - Ir	np. No. I	,Imp.	No. 2 & 3	Imp. No 4,	,Te	otal Filter	Tare Wt.		
Point #	Sample Time	Meter Vol. Vm	Vel. Head ΔP ("H2O)	Original Diff. AH ("H2O)	Stack Temp., Ts (•F)	Meter Temp., Tm (°F)	Hot Box Temp (•F)	Exit Temp. (°F)	Pump Vacuum ("Hg)	Other
_1	0	276603	104	1.55	980	72	235	62	6,0	
2	2.5	278.68	.04	1.55	982	72	236	G-1-	6.0	
3	5,0	280,53	,04	1,55	984	79	235	60	6.0	
4	7.5	282.37	,04	1,55	965	75	231	59	6.0	
5	10.0	284.17	,045	1.74	1000	78	234	57	7.0	
6	12.5	286.12	.045	1.74	1005	80	237	57	7.5	
7	15.0	288.12	,04	1.55	1001	82	241	56	7,0	
8	17,5	290.04	.045	1.74) OCS	84	2453	55	7,5	
9	20.0	292,03	,045	1.74	1012	8G_	249	55	8,0	
10	22.5	294,06	,045	1,74	1017	87	246	54	8,0	
11	25.0	296.08	,04	1,65	1012	88	249	54	8,0	
12	27.5	298.05	,04	1,55	1022	89	258	54	3.0	
13	30.0	300,00	,64	1,55	1006	90	254	53	4.0	
14	32.5	301,97	.045	1.74	1020	91	254	54	8.5	
15	35.0	303.90	.045	1.74	1021	93	258	53	9.6	
16	37.5	306,03	.045	1,74	1025	94	25 8	53	9.0	
17	40.0	300.07	1045	1.74	1028	95	258	53	9.0	
18	42.5	310.13	.045	1:74	1030	96	256	52	9.0	
19	45.0	312.18	.045	1,74	1034	94	25)	52	9.0	
20	47.5	31424	,045	1,74	1033	98	2555	53	9.5	
21	50,0	316.31	,04	1.55	1033	99	253	52	9,0	
22	52.5	318.31	.045	1,74	1036	99	252	52	9.0	
23	55,0	320.34	.045	1,74	1035	99	250	5(9,0	
24	57.5	322,40	.045	1.74	1038	[00]	248	51	9.5	
	60.0	384.49								

FIELD DATA SHEET

		LIED DATA STILL	_
Company <u>Fic</u>	st call Cri	chatory	Run No
SourceNOAA	Cremator	<u> </u>	Date <u>45/08</u>
Operator(s) MG/TN	1/DW	24 hr.	time at start <u>1722</u>
ı		24 hr.	time at end
Dimensions Dia	,(Filter 1	No(s). <u>6769</u>
LxW 0	18.5	Barom	etric Pressure ("Hg) <u>3 0, 3 9</u>
Static Press. ("H2O)	03	Elev Diff. Mano	. To Barom. (Ft.)
Meter Box No.	001	Ambient Temper	rature (F°)
Meter ∆H@	1.0150		
Meter Correction Factor	0.999	Assumptions	
Pitot Tube Cp	. 64	% Moisture 10	Sample Train Leak Check:
Nozzle ID		Stack Temp. 1000	Initial 0.609 CFM @ 15 "Hg
Nozzle Dia. (Inches)	0,600	Meter Temp. 100	Final 0.009 CFM @ 12 "Hg
Probe Length/Liner	3 quartz	Md/Ms [.04	Initial Pilot Tube (-)(+)
		K Factor 36.85	Final Pitot Tube (-) (+)

Moist. Co	ollected: - In	np. No. 1	,Imp.	No. 2 & 3	,Imp. No 4	,Те	otal Filter Tare Wt.		
Point #	Sample Time	Meter Vol.	Vel. Head ΔP ("H2O)	Original Diff. ΔH ("H2O)	Stack Temp., Ts (•F)	Meter Temp., Tm (•F)	Hot Box Temp (•F)	Exit Temp. (•F)	
1	0	331.948	,035	1.28	-932	42	237	59	

1	Sample	Meter Vol.	Vel. Head	Diff. AH	Temp., Ts	Temp.,	Hot Box	Temp.	Vacuum	
Point #	Time	Vm	ΔP ("H2O)	("H2O)	(°F)	Tm (•F)	Temp (•F)	(•F)	("Hg)	Olher
11_	10	331.948		1.28	-932	82	237	59	4,5	<u> </u>
2	2.5	333,09	,035	1.28	1005	83	238	58	- U, O	
3	5.0	33574	. 035	1,28	999	84	235	56	4.0	
4	7,5	337.40	,04	1,47	1019	85	3.30	54	3.5	
5	10.0	339,25	,035	1.28	1012	86	232	54	3.5	
6	12.5	341.00	1035	1,28	1021	87	235	53	3.5	
7	15.0	342,70	,03	1.10	1020	88	231	53	3.5	
8	17.5	344,35		1.16	1024	89	233	53	3.5	
9	20,0	345,95		(,10	1036	90	234	53	3.5	
10	22.5	347.56		.42	1038	91	235	52	3,5	
11	25,0	349.07	.03	1,10	1028	91	235	53	3.5	
12	27.5	350.69		1,10	1028	92	235	52	3.5	
13	30,6	352.34	.04	1.47	1008	91	234	52	4.5	
14	32,5	354,13	,04	1.47	1053	43	234	52	5,0	
15	35.0	355,99	,04	1,45	1057	94	236	51	5.0	
16	37.5	357.81	.04	1.47	1052	96	239	52	5.0	
17	40.0	359.68	.04	1,47	1062	96	241	52	5.5	
18	42.5	361.54	.04	1,47	1075	96	243	51	5.5	
19	45.0	363.38	,04	1,47	1083	97	245	51	5.0	
20	47.5	365.21	.035	1,28	1078	98	247	51	5.0	
21	50,0	360,99		1,76	1073	98	248	51	5.0	
22	52.5	308.77	1035	1.28	1072	98	249	50	5.0	
23	55.0	370,54	.035	1,28	1071	98	249	50	5,0	
24	57,5		.035	1.38	1059	98	245	90	6.0	
	60 0	373 701	·							

Pump

SOUTHERN ENVIRONMENTAL SCIENCES, INC. GAS ANAYLSIS DATA FORM

Plant: Roret Call Crematory	<u> </u>					
Unit: N-70 AB Crematory	Test No.:					
Date: 4/5/0%	Sampling Loc.: Sacry					
Sampling Time (24 hr. clock) 10:05 — 11:05						
Sampling Type: Continuous □ Integrated Bag ເ≮Grab □						
Analytical Method	Ambient Temp. 75					
Operator M &						

RUN→	1		2		3		Average NetVolume	Multiplier	Molecular Weight of Stack Gas(Dry Basis (MD)
	Actual		Actual		Actual]	_	
GAS	Reading	Net	Reading	Net	Reading	Net			
CO2	5.4	5.4	5,5	5.5	5,5	5.4		.44	
O2 (Net is Actual O2 Reading minus actual CO2 Reading)	18.0	126	18.2			127		.32	
CO (Net is Actual CO Reading minus actual O2 Reading)						·		.28	
N2 (Net is 1000 minus actual CO Reading)						,		.28	
								TOTAL	

SOUTHERN ENVIRONMENTAL SCIENCES, INC. GAS ANAYLSIS DATA FORM

Plant: Purst Call Crematory					
Unit: p. 20 ph arenatory	Test No.: Z				
Date: 45108	Sampling Loc.: Stack.				
Sampling Time (24 hr. clock) 13:48 - 14;48,					
Sampling Type: Continuous □ Integrated Bag 💢 Grab □					
Analytical Method Creek	Ambient Temp.				
Operator NG					

RUN→	1		2		3		Average NetVolume	Multiplier	Molecular Weight of Stack Gas(Dry Basis (MD)
	Actual		Actual		Actual			_	
GAS	Reading	Net	Reading	Net	Reading	Net			
CO2	5.1	5. i	Sil	Ŋ	o Ŵ	5.0		.44	
O2 (Net is Actual O2									
Reading minus actual CO2	17.1	120	17:1	12.0	17.1	12.1			
Reading)								.32	
CO (Net is									
Actual CO	l	l i							
Reading minus									
actual O2 Reading)								20	
N2 (Net is	 							.28	
1000 minus									
actual CO		(,				Į.			
Reading)								.28	
								TOTAL	

SOUTHERN ENVIRONMENTAL SCIENCES, INC. GAS ANAYLSIS DATA FORM

Plant: First Call Crandery,						
Unit: N. To As Crendery.	Test No.:					
Date: 415/08	Sampling Loc.: Stack					
Sampling Time (24 hr. clock) 17: ZZ 18: ZZ						
Sampling Type: Continuous □ Integrated Bag & Grab □						
Analytical Method creat Ambient Temp. 85,						
Operator M (b						

RUN→	1		2		3		Average NetVolume	Multiplier	Molecular Weight of Stack Gas(Dry Basis (MD)
	Actual		Actual		Actual			. •	
GAS	Reading	Net	Reading	Net	Reading	Net			
CO2	5.6	5.6	5.4	5.4	5.5	5,5		.44	
O2 (Net is Actual O2 Reading minus actual CO2 Reading)	18.4		18.3			13.0		.32	·
CO (Net is Actual CO Reading minus actual O2 Reading)								.28	
N2 (Net is 1000 minus actual CO Reading)						:-		.28	
						.,		TOTAL	
•							-		

SOUTHERN ENVIRONMENTAL SCIENCES, INC. NOZZLE CALIBRATION

DATE: 4/5/08 BY: M6

Nozzie ID	Run No.	D1 (in.)	D2 (in.)	D3 (in.)	ΔD (in.)	DAVG (in.)
overt 2	1-3	- 600	. 599	. 601	.002	-600

Where:

D1 D2 D3 = Nozzle diameter measured on a different

Diameter (inches).

Tolerance = 0.001 inches

= Maximum difference in any two

Measurements (inches).

Tolerance = 0.004 inches

Davg. = Average of D_1, D_2, D_3

SAMPLE POINT LOCATIONS

Company: Fiest Con Crom Atory
Source: N. Zo AA CREMATING
Date: 4/5/08
Stack/Duct Dimensions: \%⋅≤^
Port Length: Yes IX No
Points corrected for port length? 711
20"
Sketch of Stack/Duct

ΔD

Point	
No.	Distance from Duct Wall (inches)
1	7.5
2	8.2
3	912
4	10.3
	11.6
_6	13.6
7	18.9
8	20.9
વ	22.2
10	23.3
- 11	23.3 24.3
12	25.0
 	
- ` -	
 	
	

SOUTHERN ENVIRONMENTAL SCIENCES, INC. Type S Pitot Tube Inspection Form

Pitot Tube ID No.	00.INC			
Inspection Date	4/1/2002			
Inspected By	M. Gierke			
Pitot Tube Assembly Level?	Yes	No		
Pitot Tube Openings Damaged?	Yes (explain please)	No		

ANGLE	MEASUREMENT	LIMITS
•1	1 •	<10°
a2	1 •	<10•
b1	10	<5°
B2	1.0	<5°
Y	1 •	
0	2°	
Α	.290 inches	
z=A sin Y	.010 inches	<1/8 inch
$w = A \sin \theta$.021 inches	<1/32 inch
Pa	.145 inches	
Pb	.145 inches	* * / / /
. Dt	.190 inches	

COMMENTS

CALIBRATION	YES	(NO)
REQUIRED		



FUNERAL HOMES Southside Chapel

1727 Bartow Road · Lakeland, FL 33801

DEPARTMENT OF ENVIROMENTAL PROTECTION RECEIPTS
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TALLAHASSEE, FLORIDA 32315-3070

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