

F&A RECEIPT 523788

DATE: JUL 25, 2011

HUMAN CREMATORY  
AIR GENERAL PERMIT REGISTRATION FORM

Part II. Notification to Permitting Office

(Detach and submit to appropriate permitting office; keep copy onsite)

**Instructions:** To give notice to the Department of an eligible facility's intent to use this air general permit, the owner or operator of the facility must detach and complete this part of the Air General Permit Registration Form and submit it to the appropriate Department of Environmental Protection or local air pollution control program office which has permitting authority. Please type or print clearly all information, and enclose the appropriate air general permit registration processing fee pursuant to Rule 62-4.050, F.A.C. (\$100 as of the effective date of this form)

Registration Type

1310267-001

Check one:

**INITIAL REGISTRATION** - Notification of intent to:

- Construct and operate a proposed new facility.
- Operate an existing facility not currently using an air general permit (e.g., a facility proposing to go from an air operation permit to an air general permit).

**RE-REGISTRATION** (for facilities currently using an air general permit) - Notification of intent to:

- Continue operating the facility after expiration of the current term of air general permit use.
- Continue operating the facility after a change of ownership.
- Make an equipment change requiring re-registration pursuant to Rule 62-210.310(2)(e), F.A.C., or any other change not considered an administrative correction under Rule 62-210.310(2)(d), F.A.C.

Surrender of Existing Air Operation Permit(s) - For Initial Registrations Only

If the facility currently holds one or more air operation permits, such permit(s) must be surrendered by the owner or operator upon the effective date of this air general permit. In such case, check the first box, and indicate the operation permits being surrendered. If no air operation permits are held by the facility, check the second box.

- All existing air operation permits for this facility are hereby surrendered upon the effective date of this air general permit; specifically permit number(s): \_\_\_\_\_
- No air operation permits currently exist for this facility.

General Facility Information

Facility Owner/Company Name (Name of corporation, agency, or individual owner who or which owns, leases, operates, controls, or supervises the facility.)

Jerry Evans, Owner

Site Name (Name, if any, of the facility site; e.g., Plant A, Metropolis Plant, etc. If more than one facility is owned, a registration form must be completed for each.)

Evans Funeral Home

Facility Location (Provide the physical location of the facility, not necessarily the mailing address.)

Street Address: 668 Walton Rd

City: DeFuniak Springs

County: Walton

Zip Code: 32433 -3539

Received in F/A. 07/25/11

523788 RECEIVED

JUL 26 2011

DIVISION OF AIR RESOURCE MANAGEMENT

**Owner/Authorized Representative**

Name and Position Title (Person who, by signing this form below, certifies that the facility is eligible to use this air general permit.)  
 Print Name and Title: Jerry Evans, Owner

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Owner/Authorized Representative Mailing Address  
 Organization/Firm:  
 Street Address: 668 Walton Rd  
 City: DeFuniak Springs County: Walton Zip Code: 32433

---

Owner/Authorized Representative Telephone Numbers  
 Telephone: 850-951-0668 Fax:  
 Cell phone (optional):

**Facility Contact (If different from Owner/Authorized Representative)**

Name and Position Title (Plant manager or person to be contacted regarding day-to-day operations at the facility.)  
 Print Name and Title: Jerry Evans, Owner

---

Facility Contact Mailing Address  
 Organization/Firm:  
 Street Address: PO Box 668  
 City: DeFuniak Springs County: Walton Zip Code: 32435

---

Facility Contact Telephone Numbers  
 Telephone: 850-951-0668 Fax:  
 Cell phone (optional):

**Owner/Authorized Representative Statement**

This statement must be signed and dated by the person named above as owner or authorized representative

*I, the undersigned, am the owner or authorized representative of the owner or operator of the facility addressed in this Air General Permit Registration Form. I hereby certify, based on information and belief formed after reasonable inquiry, that the facility addressed in this registration form is eligible for use of this air general permit and that the statements made in this registration form are true, accurate and complete. Further, I agree to operate and maintain the facility described in this registration form so as to comply with all applicable standards for control of air pollutant emissions found in the statutes of the State of Florida and rules of the Department of Environmental Protection and revisions thereof.*

*I will promptly notify the Department of any changes to the information contained in this registration form.*

Signature Jerry Evans Date 07-26-11

### Design Calculations

If this is an initial registration for a proposed new human crematory unit, provide design calculations to confirm a sufficient volume in the secondary chamber combustion zone to provide for at least a 1.0 second gas residence time at 1800 degrees F.

- Manufacturer's' design calculations attached.  
 Registration is not for proposed new human crematory unit(s).

### Description of Facility

Below, or as an attachment to this form, provide a description of all crematory operations at the facility in sufficient detail to demonstrate the facility's eligibility for use of this air general permit and to provide a basis for tracking any future equipment or process changes at the facility. Describe all air pollutant-emitting processes and equipment at the facility, and identify any air pollution control measures or equipment used.

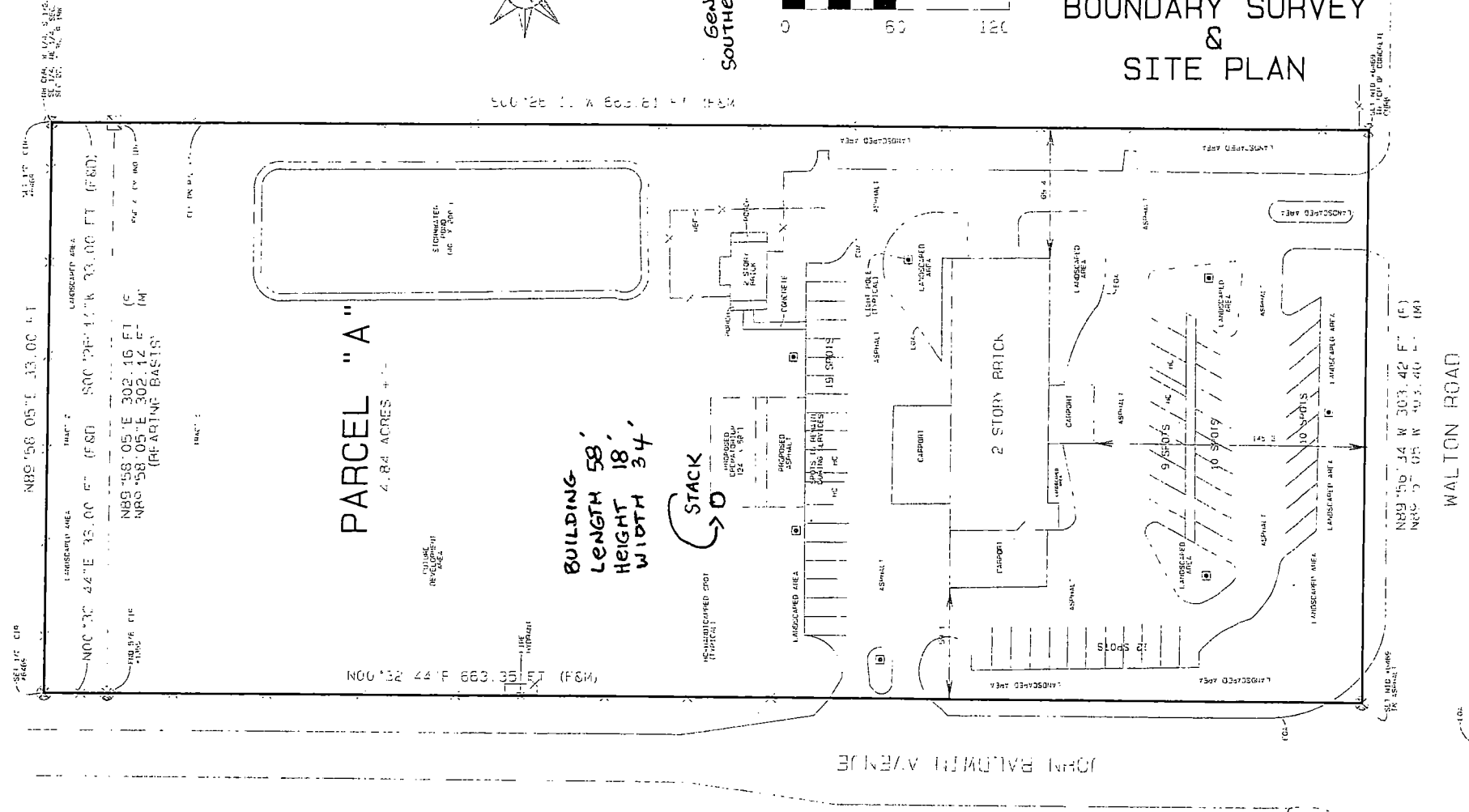
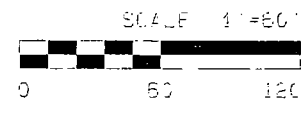
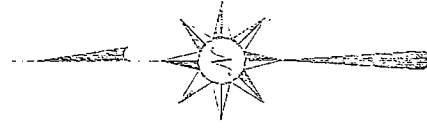
- \* 1) BEL CREMATION SYSTEMS INC
- 2) MODEL NZOSA
- 3) S/N - NOT BUILT/PURCHASED AS OF 8/18/11.
- 4) FUEL - NG ~~OR PROPANE~~
- 5) 150 LBS/HR

e-mail: evansfuneralhome@aol.com

\* ALL ABOVE INFORMATION WAS PROVIDED VIA  
TELECON W/ MR. EVANS ON 8/18/11 @ 1405 HRS  
& VERIFIED D. Wilke

Facility Start-Up Date (Estimated start-up date of proposed new facility.) (N/A for existing facility)  
8/15/2011

MAP OF  
BOUNDARY SURVEY  
&  
SITE PLAN



PARCEL "A"  
4.84 ACRES +/-

BUILDING  
LENGTH 58'  
HEIGHT 18'  
WIDTH 34'

STACK  
→

LAND ENGINEERING  
SERVICES, INC.  
P.O. BOX 49  
1031 US HWY 90W  
SUITE 3  
DEFUNIAK SPRINGS,  
FL 32435  
PHONE: 850-892-3639  
FAX: 850-892-8326  
LE#7544

CLIENT:  
EVANS FUNERAL  
HOME

CERTIFIED TO  
CLIENT

DATE OF SURVEY:  
JULY 14, 2011  
FIELD AREA CHIEF:  
JOHN JOHNSON  
PARCEL ID:  
22-24-19-19000-002-0040

SURVEY ID: 11142  
DRAWN BY:  
JOHN JOHNSON  
CHECKED BY:  
JANIE CARRO

PAGE 2 OF 2

SURVEYOR'S CERTIFICATE  
I, THE UNDERSIGNED BEING  
A LICENSED SURVEYOR AND  
BORN IN THE STATE OF  
FLORIDA, DO HEREBY CERTIFY  
THAT THE SURVEY AS SHOWN  
TO THE BEST OF MY KNOWLEDGE  
MEETS THE REQUIREMENTS OF  
THE MINIMUM TECHNICAL STANDARDS  
OF THE STATE OF FLORIDA (CHAPTER  
61G17-6, SJ-17 FLORIDA ADMINISTRATIVE  
CODE PURSUANT TO CHAPTER  
412 AND CHAPTER 161 OF THE  
FLORIDA STATUTES EXCEPT AS  
OTHERWISE NOTED

UNLESS BEARING  
EMPLOYER'S  
EMBOSSER SEAL  
7-18-11  
DATE OF SIGNATURE

JOHN JOHNSON  
FLORIDA REGISTRATION NUMBER: 6489  
FLORIDA REGISTRATION NUMBER: 57591

THIS MAP OF BOUNDARY SURVEY IS NOT FULLY  
AND COMPLETE WITHOUT THE REPORT OF BOUNDARY  
SURVEY

**EMISSIONS TESTING  
of the  
FIRST CALL CREMATORY  
B & L CREMATION SYSTEMS, INC. N20 SERIES  
HUMAN CREMATORY  
Clearwater, Florida**

April 5, 2008

FDEP Permit No. 1030473-008AG  
EU No. 008  
SES Reference No. 08S131

Conducted by:

SOUTHERN ENVIRONMENTAL SCIENCES, INC.  
1204 North Wheeler Street  
Plant City, Florida 33566  
Phone (831) 752-5014, Fax (813)752-2475

Project Participants

Byron E. Nelson  
Mark S. Gierke  
Dale A. Wingler  
Travis B. Nelson

**SPECIAL EMISSIONS**

**EMISSION TESTING**  
**of the**  
**FIRST CALL CREMATORY**  
**B & L CREMATION SYSTEMS, INC. N20 SERIES**  
**HUMAN CREMATORY**  
**Clearwater, Florida**

April 5, 2008

**TABLE OF CONTENTS**

1.0	INTRODUCTION.....	1
2.0	SUMMARY OF RESULTS.....	1
3.0	PROCESS DESCRIPTION.....	1
4.0	SAMPLING PROCESDURES.....	4
	4.1 Methods.....	4
	4.2 Sampling Locations.....	5
	4.3 Sampling Trains.....	5
	4.4 Sample Collection.....	12
	4.5 Sample Recovery.....	12
5.0	ANALYTICAL PROCEDURE.....	14
	5.1 Pretest Preparation.....	14
	5.2 Analysis.....	14
	APPENDIX.....	15
	Project Participants	
	Certification	
	Visible Emissions Evaluation	
	Process Operational Data	
	Laboratory Data	
	Field Data Sheets	
	Analyzer Strip Charts	
	Calibration Data	
	Calculations and Symbols	

## **1.0 INTRODUCTION**

Southern Environmental Sciences, Inc. conducted emissions testing of the First Call Crematory, B & L Cremation Systems, Inc. N20 Series human crematory on April 5, 2008. This facility is located at 12660 34<sup>th</sup> Street North, Clearwater, Florida. Testing was conducted for particulates, carbon monoxide (CO), sulfur dioxide (SO<sub>2</sub>), nitrogen oxides (NO<sub>x</sub>), total hydrocarbons (VOC) and visible emissions. Oxygen (O<sub>2</sub>) concentrations were measured to correct emission rates to 7% O<sub>2</sub>. Mr. Jose Rodriguez of the Pinellas County Department of Environmental Management was present as an observer during a portion of the testing.

## **2.0 SUMMARY OF RESULTS**

Results of the particulate, carbon monoxide, sulfur dioxide, nitrogen oxides and total hydrocarbons are summarized in Table 1. A visible emissions evaluation was performed over a one hour period. The average maximum six minute opacity was zero percent.

## **3.0 PROCESS DESCRIPTION**

The B & L Cremation Systems N20 Series crematory incinerator cremates human remains in an environmentally acceptable manner. The unit consists of a primary and secondary (afterburner) chamber each fired with natural gas. The unit is designed to incinerate human remains at a rate of 150 pounds per hour with a maximum heat input rate of 1.5 MMBTU per hour (primary chamber 0.5 MMBTU per hour, secondary chamber 1.0 MMBTU per hour).



**TABLE 1. EMISSIONS TEST SUMMARY****Company: FIRST CALL CREMATORY****Source: B & L Cremation Systems, Inc.****N20 Series Human Crematory**

	<b>Run 1</b>	<b>Run 2</b>	<b>Run 3</b>
Date of Run	4/5/08	4/5/08	4/5/08
Weight of Human Remains (lbs.)	170	165	140
Start Time (24-hr. clock)	1005	1348	1722
End Time (24-hr. clock)	1107	1452	1824
Vol. Dry Gas Sampled Meter Cond. (DCF)	39.324	47.848	41.832
Gas Meter Calibration Factor	0.994	0.994	0.994
Barometric Pressure at Barom. (in. Hg.)	30.39	30.29	30.39
Elev. Diff. Manom. To Barom. (ft.)	0	0	0
Vol. Liquid Collected Std. Cond. (SCF)	3.305	5.073	2.966
Moisture in Stack Gas (% Vol.)	7.8	9.9	8.6
Molecular Weight Wet Stack Gas	28.48	28.17	28.62
Stack Gas Static Press. (in. H <sub>2</sub> O gauge)	-0.03	-0.03	-0.03
Average Square Root Velocity Head	0.166	0.208	0.187
Average Orifice Differential (in. H <sub>2</sub> O)	1.132	1.669	1.291
Average Gas Meter Temperature (°F)	81.5	88.3	91.7
Average Stack Gas Temperature (°F)	834.3	1013.6	998.3
Pilot Tube Coefficient	0.84	0.84	0.84
Stack Gas Vel. Stack Cond. (ft./sec.)	16.78	19.88	17.65
Effective Stack Area (sq. ft.)	1.87	1.87	1.87
Stack Gas Flow Rate Std. Cond. (DSCFM)	623	715	659
Stack Gas Flow Rate Stack Cond. (ACFM)	1,833	2,202	1,977
Net Time of Run (min.)	60	60	60
Nozzle Diameter (in.)	0.600	0.600	0.600
Percent Isokinetic	98.7	102.6	97.6

**TABLE 1. EMISSIONS TEST SUMMARY (con't)**

**Company:** FIRST CALL CREMATORY  
**Source:** B&L Cremation Systems, Inc.  
 N20 Series Human Crematory

	<b>Run 1</b>	<b>Run 2</b>	<b>Run 3</b>	
Date of Run	4/5/08	4/5/08	4/5/08	
Weight of Human Remains (lbs.)	170	165	140	
Start Time (24 hr. clock)	1005	1348	1722	
End Time (24 hr. clock)	1107	1452	1824	
Oxygen (%)	12.7	12.1	13.1	
Particulate Collected (mg.)	27.0	69.1	99.2	
			<b>(Avg.)</b>	
Particulate Emissions (gr./DSCF)	0.011	0.023	0.038	0.024
Particulate Emissions (gr./DSCF @ 7% O2)	0.018	0.036	0.066	0.040
Particulate Emissions (lb./hr.)	0.06	0.14	0.21	0.136
CO Emissions (ppm)	3.05	2.27	4.98	3.43
CO Emissions (ppm @ 7% O2)	3.4	2.95	6.7	4.35
CO Emissions (lb./hr.)	0.007	0.006	0.018	0.010
NOx Emissions (ppm)	110.23	122.3	115.7	116.1
NOx Emissions (lb./hr.)	0.58	0.71	0.74	0.677
VOC Emissions (ppm)	1.5	0.80	1.41	1.237
VOC Emissions (lb./hr.)	0.007	0.004	0.009	0.007
SO2 Collected (mg)	33.1	49.4	59.7	47.4
SO2 Emissions (lb./hr.)	0.088	0.142	0.167	0.13

Note: Standard conditions 68°F, 29.92 in. Hg

1.0 MMBTU/hr.). Emissions are controlled by the afterburner that is preheated and maintained at a minimum operating temperature of 1600°F prior to and during ignition of the primary chamber. Process operational data was provided by facility personnel and is included in the appendix.

## 4.0 SAMPLING PROCEDURES

### 4.1 Methods

All sampling was performed using methods currently acceptable to the FDEP. All test methods are contained in Title 40 of the Code of Federal Regulations, Appendix A and are as follows:

<u>Pollutant</u>	<u>EPA Method No.</u>	<u>Title</u>
Particulates	5	Determination of Particulate Emissions from Stationary Sources
Carbon Monoxide	10	Determination of Carbon Monoxide Emissions from Stationary Sources
Oxygen	3B	Gas analysis for the Determination of Emissions Rate Correction Factor or Excess Air
Nitrogen Oxides	7E	Determination of Nitrogen Oxides Emissions from Stationary Sources (Instrumental Analyzer Procedure)
Sulfur Dioxide	6	Determination of Sulfur Dioxide Emissions from Stationary Sources, Section 2.1
Total Hydrocarbons	25A	Determination of Total Gaseous Organic Concentration Using a Flame Ionization Analyzer
Visible Emissions	9	Visual Determination of the Opacity of Emissions of Stationary Sources.

Sulfur dioxide emissions were determined simultaneous with particulates as per Section 6.1 of EPA Method 6.

#### **4.2 Sampling Locations**

Locations of the sample ports and stack dimensions are shown in Figure 1.

Particulate/SO<sub>2</sub> sampling was accomplished by conducting horizontal traverses through each of two ports located on the stack at a ninety degree angle from one another. Twenty four sample points were chosen in accordance with EPA Method 1 – Sample and Velocity Traverses for Stationary Sources, 40 CFR 60, Appendix A. Carbon monoxide, nitrogen oxides, total hydrocarbon and oxygen sampling were performed from the same sampling ports as the particulate/SO<sub>2</sub> sampling.

#### **4.3 Sampling Trains**

The particulate/SO<sub>2</sub> sampling train consisted of a 3 foot Inconel probe utilizing a one piece quartz glass nozzle and liner, a heated glass fiber filter and four impingers arranged as shown in Figure 2. Flexible tubing was used between the heated filter and the impingers. The first impinger was charged with 100 milliliters of 80% isopropanol, the second and third impingers were each charged with 100 milliliters of a 3% percent hydrogen peroxide solution and the fourth impinger was charged with indicating silica gel desiccant. The impingers were cooled in an ice and water bath during sampling. A Nutech Corporation control console was used to monitor the gas flow rates and stack conditions during sampling.

The carbon monoxide sampling train consisted of a stainless steel probe, Teflon sample line, condenser, silica gel and carbon dioxide adsorbent tubes and a Thermo Environmental Instruments, Inc. Model 48 Gas Filter Correlation CO analyzer arranged as shown in Figure 3.

The nitrogen oxides sampling train consisted of a stainless steel probe, Teflon sample line, and a California Analytical Inc. Model 300 FID analyzer arranged as shown in Figure 5.

The oxygen sampling train consisted of a probe, sample line, tedlar bag in a rigid container, valve, vacuum pump, and flow meter.

#### **4.4 Sample Collection**

Prior to particulate/SO<sub>2</sub> sampling, the pitot tubes were checked for leaks and the manometers were zeroed. A pretest leak check of the sampling train was conducted by sealing the nozzle and applying a 15" Hg vacuum. A leak rate of less than 0.02 cubic feet per minute was considered acceptable. Sample was collected isokinetically for two and one half minutes at each of the points sampled.

All instrumental analyzers were calibrated immediately prior to the beginning and checked after each run by introducing known gases into the instrument through the sampling.

The tedlar bag used for obtaining an integrated oxygen sample was leak checked prior to the test by pressurizing it to 2 to 4 in. H<sub>2</sub>O and allowing it to stand overnight. The bag was considered leak free if it remained inflated. A one hour integrated sample was obtained at a rate 0.5 liters per minute for each run.

All sampling was conducted simultaneously.

#### **4.5 Sample Recovery**

A post test leak check of the particulate/SO<sub>2</sub> sampling train was performed at the completion of each run by sealing the nozzle and applying a vacuum equal to or greater than the maximum value reached during the sample period. A leak rate of less than 0.02 CFM or 4 percent of the average sampling rate (whichever was less) was considered acceptable. The probe was then disconnected, the ice bath was drained and the remaining part of the sampling train was purged by drawing charcoal filtered air through the system for fifteen minutes at the average flow rate used during sampling. The nozzle and probe were then brushed and rinsed with reagent grade acetone and the washings were placed in clean polyethylene containers and sealed. The glass fiber filter was removed from the holder with forceps and placed in a covered Petri dish for return to the laboratory. The front half of the filter holder was rinsed with acetone and the washings were added to the nozzle and probe wash. The contents of impingers 1 through 3 were measured volumetrically and the silica gel in the fourth impinger was weighed to the nearest 0.1 gram for determination of moisture content. The 80 percent isopropanol in the first

impinger was discarded and the impinger was rinsed with deionized, distilled water. The 3 percent hydrogen peroxide in the second and third impingers was placed in a clean polyethylene sample bottle. The impingers, associated glassware and back half of the filter holder were then rinsed with de-ionized, distilled water which was added to the sample bottle.

Two calculations of the moisture content of the stack gas were made for each run, one from the impinger analysis and one from the assumption of saturated conditions based upon the average stack gas temperature and a psychrometric chart as described in EPA Method 4, Determination of Moisture Content in Stack Gases, 40 CFR 60, Appendix A. The lower of the two values of moisture content was considered to be correct and was used in the emissions computations.

## **5.0 ANALYTICAL PROCEDURE**

### **5.1 Pretest Preparation**

The glass fiber filters for the particulate train were numbered, oven dried at 105°C for two to three hours, desiccated and weighed to a constant weight in preparation for the test. Results were recorded to the nearest 0.1 milligram. Filters were loaded into holders and a filter was set aside as a control blank. The impingers were charged as described in section 4.3 and the contents of the fourth impinger were weighed to the nearest 0.1 gram. The 3 percent hydrogen peroxide solution for the sulfur dioxide sampling was prepared the morning of the test from 30 percent reagent grade stock solution.

## 5.2 Analysis

Upon return to the laboratory, the particulate filters were removed from the containers with forceps, dried at 105°C for two to three hours, desiccated and weighed to a constant weight. Results were recorded to the nearest 0.1 milligram. The probe and nozzle washes and an acetone blank were measured volumetrically and transferred to clean, tared evaporating dishes and evaporated to dryness over low heat. The evaporating dishes were then oven dried at 105°C for two to three hours, desiccated and weighed to a constant weight. Results were recorded to the nearest 0.1 milligram. The total particulate reported is the sum of the filter weight gain and the weight gain of the evaporating dishes, corrected for the acetone blank. The impinger solutions were analyzed for sulfur dioxide procedures specified in Section 4.3 of EPA Method 8.



**PROJECT PARTICIPANTS AND CERTIFICATION**

**FIRST CALL CREMATORY  
B & L CREMATION SYSTEMS, INC. N20 SERIES  
HUMAN CREMATORY  
Clearwater, Florida**

April 5, 2008


**Project Participants:**

Marke S. Gierke  
Byron E. Nelson  
Dale A. Wingler  
Travis B. Nelson

Kenneth M. Roberts

**Certification:**

I certify that to my knowledge all data submitted in this report is true and correct.

  
Byron E. Nelson, CIH

# Southern Environmental Sciences, Inc.

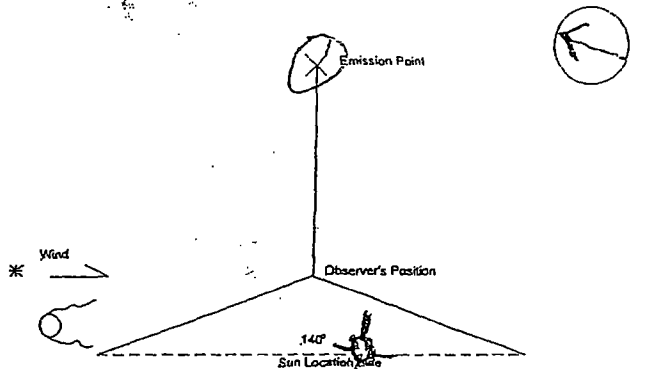
1204 North Wheeler Street □ Plant City, Florida 33563 □ (813) 752-5014, Fax (813) 752-2475

## VISIBLE EMISSIONS EVALUATION

COMPANY <i>First Call Crematory</i>	
UNIT <i>N20 AA Crematory Incinerator</i>	
ADDRESS <i>12660 34th St. N #A-1</i> <i>Clearwater, FL</i>	
PERMIT NO. <i>1030473-003-AG</i>	COMPLIANCE? YES <input checked="" type="checkbox"/> NO <input type="checkbox"/>
AIRS NO. <i>1030473</i>	EU NO. <i>001</i>
PROCESS RATE <i>160 lb Body</i>	PERMITTED RATE <i>Adult Size Body - (150 lb/hr)</i>
PROCESS EQUIPMENT <i>B&amp;L N20 AA Crematory Incinerator</i>	
CONTROL EQUIPMENT <i>Affor burner</i>	
OPERATING MODE <i>Nat. Gas Fired</i>	AMBIENT TEMP. (° F) START <i>85</i> STOP <i>85</i>
HEIGHT ABOVE GROUND LEVEL START <i>130'</i> STOP <i>same</i>	HEIGHT RELATIVE TO OBSERVER START <i>130'</i> STOP <i>same</i>
DISTANCE FROM OBSERVER START <i>190'</i> STOP <i>same</i>	DIRECTION FROM OBSERVER START <i>50°</i> STOP <i>50°</i>
EMISSION COLOR <i>NONE</i>	PLUME TYPE <i>N/A</i> CONTIN. <input type="checkbox"/> INTERMITTENT <input type="checkbox"/>
WATER DROPLETS PRESENT? NO <input checked="" type="checkbox"/> YES <input type="checkbox"/>	IS WATER DROPLET PLUME ATTACHED <input type="checkbox"/> DETACHED <input type="checkbox"/> <i>N/A</i>
POINT IN PLUME AT WHICH OPACITY WAS DETERMINED START <i>Stack Exit</i> STOP <i>same</i>	
DESCRIBE BACKGROUND START <i>sky</i> STOP <i>sky</i>	
BACKGROUND COLOR START <i>bl/wh</i> STOP <i>same</i>	SKY CONDITIONS START <i>scattered</i> STOP <i>same</i>
WIND SPEED (MPH) START <i>0-10</i> STOP <i>same</i>	WIND DIRECTION START <i>Var.</i> STOP <i>Var.</i>
AVERAGE OPACITY FOR HIGHEST PERIOD <i>0%</i>	RANGE OF OPACITY READINGS MIN. <i>0</i> MAX. <i>0</i>

SOURCE LAYOUT SKETCH

Draw North Arrow



Comments

OBSERVATION DATE <i>4/5/08</i>					START TIME <i>1348</i>					STOP TIME <i>1448</i>				
SEC MIN					SEC MIN					SEC MIN				
	0	15	30	45		0	15	30	45		0	15	30	45
0	0	0	0	0	30	0	0	0	0	0	0	0	0	
1	0	0	0	0	31	0	0	0	0	0	0	0	0	
2	0	0	0	0	32	0	0	0	0	0	0	0	0	
3	0	0	0	0	33	0	0	0	0	0	0	0	0	
4	0	0	0	0	34	0	0	0	0	0	0	0	0	
5	0	0	0	0	35	0	0	0	0	0	0	0	0	
6	0	0	0	0	36	0	0	0	0	0	0	0	0	
7	0	0	0	0	37	0	0	0	0	0	0	0	0	
8	0	0	0	0	38	0	0	0	0	0	0	0	0	
9	0	0	0	0	39	0	0	0	0	0	0	0	0	
10	0	0	0	0	40	0	0	0	0	0	0	0	0	
11	0	0	0	0	41	0	0	0	0	0	0	0	0	
12	0	0	0	0	42	0	0	0	0	0	0	0	0	
13	0	0	0	0	43	0	0	0	0	0	0	0	0	
14	0	0	0	0	44	0	0	0	0	0	0	0	0	
15	0	0	0	0	45	0	0	0	0	0	0	0	0	
16	0	0	0	0	46	0	0	0	0	0	0	0	0	
17	0	0	0	0	47	0	0	0	0	0	0	0	0	
18	0	0	0	0	48	0	0	0	0	0	0	0	0	
19	0	0	0	0	49	0	0	0	0	0	0	0	0	
20	0	0	0	0	50	0	0	0	0	0	0	0	0	
21	0	0	0	0	51	0	0	0	0	0	0	0	0	
22	0	0	0	0	52	0	0	0	0	0	0	0	0	
23	0	0	0	0	53	0	0	0	0	0	0	0	0	
24	0	0	0	0	54	0	0	0	0	0	0	0	0	
25	0	0	0	0	55	0	0	0	0	0	0	0	0	
26	0	0	0	0	56	0	0	0	0	0	0	0	0	
27	0	0	0	0	57	0	0	0	0	0	0	0	0	
28	0	0	0	0	58	0	0	0	0	0	0	0	0	
29	0	0	0	0	59	0	0	0	0	0	0	0	0	

OBSERVER: *Mark Gierke*

Certified by: *ENG* <sup>thru</sup> *EAH* Certif. #

Certified at: *Tampa, FL*

Date Certified: *2/08*

Exp. Date: *8/08*

I certify that all data provided to the person conducting the test was true and correct to the best of my knowledge:

Signature: *See Process Wt. Statement*

Title:

Process Weight Statement

DATE 4/5/08 SAMPLING TIME: FROM 10:05 A.M. TO 6:24 P.M.

**STATEMENT OF PROCESS WEIGHT**

COMPANY	First Call Crematory.
MAILING ADDRESS	12660 34 <sup>TH</sup> ST. N. CLEARWATER FL
SOURCE IDENTIFICATION	B&L SYSTEMS N-20 SERIES CREMATORY.
SOURCE LOCATION	12660 34 <sup>TH</sup> ST. N. CLEARWATER FL

**DATA ON OPERATING CYCLE TIME**

START OF OPERATION, TIME		
END OF OPERATION, TIME		
ELAPSED TIME		
IDLE TIME DURING CYCLE		
DESIGN PROCESS RATING	PROCESS WEIGHT RATE (INPUT)	150 lb/hr
	PRODUCT (OUTPUT)	

**DATA ON ACTUAL PROCESS RATE DURING OPERATION CYCLE**

MATERIAL	Human Remains	RATE	160 lbs (Run 1)
MATERIAL	" "	RATE	155 lbs (Run 2)
MATERIAL	" "	RATE	140 lbs (Run 3)
AVERAGE PROCESS WEIGHT		RATE	
PRODUCT		RATE	
PRODUCT		RATE	
PRODUCT		RATE	

I certify that the above information is true and correct to the best of my knowledge.  
Name (Please Print)

Signature \_\_\_\_\_

Title operator.

SOUTHERN ENVIRONMENTAL SCIENCES, INC.

PARTICULATE MATTER COLLECTED

PLANT: FIRST CALL CREMATORY  
 UNIT NO.: B & L CREMATION SYSTEMS, INC. - N20 SERIES HUMAN CREMATORY  
 TEST DATE: 4/5/08

ANALYZED BY: MG

Acetone blank container no.	405	Filter blank no.	6752
Acetone blank volume, ml., (VA)	200	Filter blank tare weight, g.	0.3402
Acetone blank final weight, g.	101.0509	Filter blank final weight, g.	0.3409
Acetone blank tare weight, g.	101.0507	Filter weight diff., g.	0.0007
Acetone blank weight diff., g. (ma)	0.00012		

Run No.	1	<table border="1"> <thead> <tr> <th>Container Number</th> <th colspan="3">Weight of Particulate Collected</th> </tr> <tr> <td></td> <th>Final Weight</th> <th>Tare Weight</th> <th>Weight Gain</th> </tr> </thead> <tbody> <tr> <td>1 (Filter)</td> <td>0.3603</td> <td>0.3434</td> <td>0.0169</td> </tr> <tr> <td>2 (Wash)</td> <td>103.1076</td> <td>105.6522</td> <td>0.0102</td> </tr> <tr> <td colspan="2"></td> <td>Total</td> <td>0.0271</td> </tr> <tr> <td colspan="2"></td> <td>Less acetone blank, g. (Wa)</td> <td>0.0001</td> </tr> <tr> <td colspan="2"></td> <td>Weight of particulate matter, g</td> <td>0.0270</td> </tr> </tbody> </table>			Container Number	Weight of Particulate Collected				Final Weight	Tare Weight	Weight Gain	1 (Filter)	0.3603	0.3434	0.0169	2 (Wash)	103.1076	105.6522	0.0102			Total	0.0271			Less acetone blank, g. (Wa)	0.0001			Weight of particulate matter, g	0.0270
Container Number	Weight of Particulate Collected																															
	Final Weight	Tare Weight	Weight Gain																													
1 (Filter)	0.3603	0.3434	0.0169																													
2 (Wash)	103.1076	105.6522	0.0102																													
		Total	0.0271																													
		Less acetone blank, g. (Wa)	0.0001																													
		Weight of particulate matter, g	0.0270																													
Filter No.	6768																															
Liquid lost during transport	0																															
Acetone wash volume, ml (Vaw)	100																															
Acetone wash residue, g.(Wa)	0.0001																															
Acetone wash container no.	4																															

Run No.	2	<table border="1"> <thead> <tr> <th>Container Number</th> <th colspan="3">Weight of Particulate Collected</th> </tr> <tr> <td></td> <th>Final Weight</th> <th>Tare Weight</th> <th>Weight Gain</th> </tr> </thead> <tbody> <tr> <td>1 (Filter)</td> <td>0.3972</td> <td>0.3391</td> <td>0.0581</td> </tr> <tr> <td>2 (Wash)</td> <td>105.6633</td> <td>105.6522</td> <td>0.0111</td> </tr> <tr> <td colspan="2"></td> <td>Total</td> <td>0.0692</td> </tr> <tr> <td colspan="2"></td> <td>Less acetone blank, g. (Wa)</td> <td>0.0001</td> </tr> <tr> <td colspan="2"></td> <td>Weight of particulate matter, g</td> <td>0.0691</td> </tr> </tbody> </table>			Container Number	Weight of Particulate Collected				Final Weight	Tare Weight	Weight Gain	1 (Filter)	0.3972	0.3391	0.0581	2 (Wash)	105.6633	105.6522	0.0111			Total	0.0692			Less acetone blank, g. (Wa)	0.0001			Weight of particulate matter, g	0.0691
Container Number	Weight of Particulate Collected																															
	Final Weight	Tare Weight	Weight Gain																													
1 (Filter)	0.3972	0.3391	0.0581																													
2 (Wash)	105.6633	105.6522	0.0111																													
		Total	0.0692																													
		Less acetone blank, g. (Wa)	0.0001																													
		Weight of particulate matter, g	0.0691																													
Filter No.	6770																															
Liquid lost during transport, ml.	0																															
Acetone wash container no.	18																															
Acetone wash volume, ml (Vaw)	125																															
Acetone wash residue, g.(Wa)	0.0001																															

Run No.	3	<table border="1"> <thead> <tr> <th>Container Number</th> <th colspan="3">Weight of Particulate Collected</th> </tr> <tr> <td></td> <th>Final Weight</th> <th>Tare Weight</th> <th>Weight Gain</th> </tr> </thead> <tbody> <tr> <td>1 (Filter)</td> <td>0.4182</td> <td>0.3373</td> <td>0.0362</td> </tr> <tr> <td>2 (Wash)</td> <td>100.6350</td> <td>100.6166</td> <td>0.0184</td> </tr> <tr> <td colspan="2"></td> <td>Total</td> <td>0.0993</td> </tr> <tr> <td colspan="2"></td> <td>Less acetone blank, g. (Wa)</td> <td>0.0001</td> </tr> <tr> <td colspan="2"></td> <td>Weight of particulate matter, g</td> <td>0.0992</td> </tr> </tbody> </table>			Container Number	Weight of Particulate Collected				Final Weight	Tare Weight	Weight Gain	1 (Filter)	0.4182	0.3373	0.0362	2 (Wash)	100.6350	100.6166	0.0184			Total	0.0993			Less acetone blank, g. (Wa)	0.0001			Weight of particulate matter, g	0.0992
Container Number	Weight of Particulate Collected																															
	Final Weight	Tare Weight	Weight Gain																													
1 (Filter)	0.4182	0.3373	0.0362																													
2 (Wash)	100.6350	100.6166	0.0184																													
		Total	0.0993																													
		Less acetone blank, g. (Wa)	0.0001																													
		Weight of particulate matter, g	0.0992																													
Filter No.	6769																															
Liquid lost during transport, ml.	0																															
Acetone wash container no.	53																															
Acetone wash volume, ml (Vaw)	130																															
Acetone wash residue, g.(Wa)	0.0001																															

SOUTHERN ENVIRONMENTAL SCIENCES, INC.

MOISTURE COLLECTED

Plant FIRST COU CREMATORY

Unit NZOAA Crematory

Date 4/5/08

Run No. 1

Impinger Number	1	2	3	4	Weighed by:
Final Weight (g):	<u>160.0</u>	<u>104.0</u>	<u>0</u>	<u>259.4</u>	<u>DW</u>
Initial Weight (g):	<u>100.0</u>	<u>100.0</u>	<u>0</u>	<u>253.3</u>	<u>DW</u>
Difference (g):	<u>60.0</u>	<u>4.0</u>	<u>0</u>	<u>6.1</u>	
Total Condensate (g):				<u>70.1</u>	

Unit CREMATORY

Date 4/5/08

Run No. 2

Impinger Number	1	2	3	4	Weighed by:
Final Weight (grams)	<u>195.0</u>	<u>105.0</u>	<u>0</u>	<u>266.8</u>	<u>DW</u>
Initial Weight (grams)	<u>100.0</u>	<u>100.0</u>	<u>0</u>	<u>259.2</u>	<u>DW</u>
Difference (grams)	<u>95.0</u>	<u>5.0</u>	<u>0</u>	<u>7.6</u>	
Total Condensate (grams)				<u>107.6</u>	

Unit CREMATORY

Date 4/5/08

Run # 3

Impinger Number	1	2	3	4	Weighed by:
Final Weight	<u>144.0</u>	<u>110.0</u>	<u>0</u>	<u>263.2</u>	<u>DW</u>
Initial Weight (grams)	<u>100.0</u>	<u>100.0</u>	<u>0</u>	<u>254.3</u>	<u>DW</u>
Difference (grams)	<u>44.0</u>	<u>10.0</u>	<u>0</u>	<u>8.9</u>	
Total Condensate (grams)				<u>62.9</u>	









SOUTHERN ENVIRONMENTAL SCIENCES, INC.  
GAS ANALYSIS DATA FORM

Plant: <u>Forest Hill Crematory</u>	
Unit: <u>N-20 AA Crematory</u>	Test No.: <u>1</u>
Date: <u>4/5/08</u>	Sampling Loc.: <u>Stack</u>
Sampling Time (24 hr. clock) <u>10:05 - 11:05</u>	
Sampling Type: Continuous <input type="checkbox"/> Integrated Bag <input checked="" type="checkbox"/> Grab <input type="checkbox"/>	
Analytical Method <u>Orsat</u>	Ambient Temp. <u>75</u>
Operator <u>MS</u>	

RUN→	1		2		3		Average NetVolume	Multiplier	Molecular Weight of Stack Gas(Dry Basis (MD))
	Actual Reading	Net	Actual Reading	Net	Actual Reading	Net			
CO2	5.4	5.4	5.5	5.5	5.5	5.4		.44	
O2 (Net is Actual O2 Reading minus actual CO2 Reading)	18.0	12.6	18.2	12.7	18.1	12.7		.32	
CO (Net is Actual CO Reading minus actual O2 Reading)								.28	
N2 (Net is 1000 minus actual CO Reading)								.28	
								TOTAL	

SOUTHERN ENVIRONMENTAL SCIENCES, INC.  
GAS ANALYSIS DATA FORM

Plant: <u>First Call Crematory</u>	
Unit: <u>N-20 SA Crematory</u>	Test No.: <u>2</u>
Date: <u>4/15/08</u>	Sampling Loc.: <u>Stack</u>
Sampling Time (24 hr. clock) <u>13:48 - 14:48</u>	
Sampling Type: Continuous <input type="checkbox"/> Integrated Bag <input checked="" type="checkbox"/> Grab <input type="checkbox"/>	
Analytical Method <u>Oxstat</u>	Ambient Temp. <u>80</u>
Operator <u>MG</u>	

RUN→	1		2		3		Average NetVolume	Multiplier	Molecular Weight of Stack Gas(Dry Basis (MD))
	Actual Reading	Net	Actual Reading	Net	Actual Reading	Net			
CO2	5.1	5.1	5.1	5.1	5.0	5.0		.44	
O2 (Net is Actual O2 Reading minus actual CO2 Reading)	17.1	12.0	17.1	12.0	17.1	12.1		.32	
CO (Net is Actual CO Reading minus actual O2 Reading)								.28	
N2 (Net is 1000 minus actual CO Reading)								.28	
								TOTAL	

SOUTHERN ENVIRONMENTAL SCIENCES, INC.  
GAS ANALYSIS DATA FORM

Plant: <u>Purist Cell Bromberg,</u>	
Unit: <u>N. 70th Ave Bromberg,</u>	Test No.: <u>3</u>
Date: <u>4/5/08</u>	Sampling Loc.: <u>Stack</u>
Sampling Time (24 hr. clock) <u>17:22-18:22</u>	
Sampling Type: Continuous <input type="checkbox"/> Integrated Bag <input checked="" type="checkbox"/> Grab <input type="checkbox"/>	
Analytical Method <u>Orsat</u>	Ambient Temp. <u>85</u>
Operator <u>MB</u>	

RUN→	1		2		3		Average Net Volume	Multiplier	Molecular Weight of Stack Gas(Dry Basis (MD))
	Actual Reading	Net	Actual Reading	Net	Actual Reading	Net			
CO2	<u>5.6</u>	<u>5.6</u>	<u>5.4</u>	<u>5.4</u>	<u>5.5</u>	<u>5.5</u>		<u>.44</u>	
O2 (Net is Actual O2 Reading minus actual CO2 Reading)	<u>18.4</u>	<u>12.8</u>	<u>18.3</u>	<u>12.9</u>	<u>18.5</u>	<u>13.0</u>		<u>.32</u>	
CO (Net is Actual CO Reading minus actual O2 Reading)								<u>.28</u>	
N2 (Net is 1000 minus actual CO Reading)								<u>.28</u>	
								<u>TOTAL</u>	



SOUTHERN ENVIRONMENTAL SCIENCES, INC.  
Type S Pitot Tube Inspection Form

Pitot Tube ID No.	00.INC	
Inspection Date	4/1/2002	
Inspected By	M. Gierke	
Pitot Tube Assembly Level?	<input checked="" type="radio"/> Yes	<input type="radio"/> No
Pitot Tube Openings Damaged?	Yes (explain please)	<input checked="" type="radio"/> No

ANGLE	MEASUREMENT	LIMITS
o1	1°	<10°
a2	1°	<10°
b1	1°	<5°
B2	1°	<5°
Y	1°	
0	2°	
A	.290 inches	
$z = A \sin Y$	.010 inches	<1/8 inch
$w = A \sin 0$	.021 inches	<1/32 inch
Pa	.145 inches	
Pb	.145 inches	
Dt	.190 inches	

COMMENTS

CALIBRATION REQUIRED	YES	<input checked="" type="radio"/> NO
-------------------------	-----	-------------------------------------

**CALCULATIONS FOR PRODUCTS OF COMBUSTION  
AND RESIDENCE TIME FOR 150 LB/hr  
TYPE IV WASTE. B&L N-20 SERIES CREMATORY**

**PROPANE**

**A. BASIS: 1 LB WASTE**

- |  |                                   |
|--|-----------------------------------|
| 1. $\frac{1 \text{ lb waste} \times 1000 \text{ Btu/lb waste} \times 15 \text{ lbs air}}{10,000 \text{ Btu}}$  | = 1.5 lbs air                     |
| 2. $\frac{1 \text{ lb waste} \times 0.10 \text{ lb combustible}}{1 \text{ lb waste}}$  | = 0.10 lbs of combustibles        |
| 3. $\frac{1 \text{ lb waste} \times 0.85 \text{ lb H}_2\text{O} \times 1.6^*}{1 \text{ lb waste}}$   | = 1.36 lbs of water               |
| 4. $\frac{6,500 \text{ Btu aux fuel}^{**} \times 23.8 \text{ cu ft air/cu ft fuel}}{2,500 \text{ Btu/cu ft fuel} \times 13.35 \text{ cu ft air/lb air @ 70f}}$ | = 4.64 lbs of air for aux fuel    |
| 5. $\frac{6,500 \text{ Btu aux fuel} \times 0.044 \text{ lb fuel/cu ft fuel}}{2,500 \text{ Btu/cu ft fuel}}$   | = 0.11 lb of aux fuel             |
| 6. Sum = PRODUCTS OF COMBUSTION (POC)  | = 7.71 lbs POC per lb waste @ 70f |

**B. RESIDENCE TIME @ 1600 F**

1.  $\frac{7.71 \text{ lbs POC/lbs waste} \times 51.89 \text{ cu ft / lb POC @ 1600f} \times 150 \text{ lbs waste / hr}}{3600 \text{ sec/hr}}$
- = 16.67 cu ft / sec @ 1600 f = 17.00 cu ft for 1 second residence time

**RESIDENCE TIME @ 1800 F**

2.  $\frac{7.71 \text{ lbs POC/lbs waste} \times 56.93 \text{ cu ft / lb POC @ 1800f} \times 150 \text{ lbs waste / hr}}{3600 \text{ sec/hr}}$
- = 18.1 cu ft / sec @ 1800 f = 19.00 cu ft for 1 second residence time

\* Correction multiplier for dry air and water vapor

\*\* Fuel is propane

Referances: Incinerator institute of America.  
North American Combustion Handbook  
Eclipse Combustion Engineering guide

**C. THERMOCOUPLE PLACEMENT.**

Secondary chamber operating temperature at > or = to 1600f = 17.00 cu ft from flame tip.  
1800f = 19.00 cu ft from flame tip.



Cremation  
*Systems, Inc.*

7205 - 114th Avenue North • Largo, Florida 33773  
1-800-622-5411 • 727-541-4666 • Facsimile 727-547-0669  
e-mail: blcremsys@aol.com • www.blcremationsystems.com

## PROCESS DESCRIPTION

This project consists of the construction of one new cremation retort. This crematorium will consist of one B & L Systems Model N-20SA Human Cremator. The cremation unit will be fired on propane.

Deceased human remains are manually placed into the primary chamber of the cremator. The door of the cremator is then closed. After a preheat of the afterburning chambers by the auxiliary burner, initial and supplementary combustion is provided by propane fired burner located in the primary chamber of the cremator. Once material combustion is initiated, the rate of the combustion is controlled by limiting both the combustion air and fuel supplied to the primary chamber through the primary burner. This process generates a highly combustible gas mixture that flows into a secondary chamber where more air is admitted to insure further oxidation of the gases. The auxiliary burner is installed in the secondary chamber of the cremator to facilitate complete combustion of all gaseous materials entering this chamber.

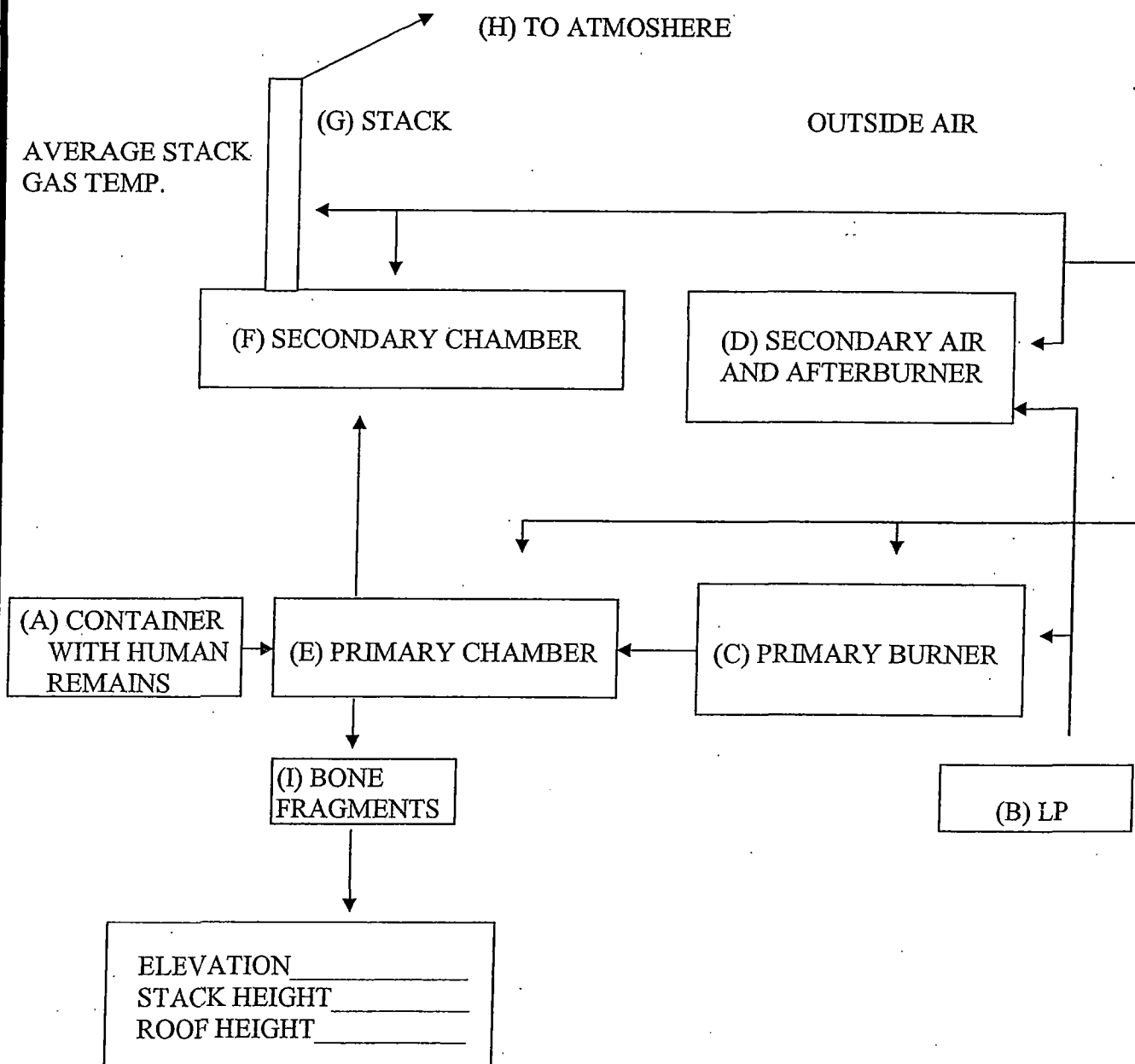
Once the cremation process is complete, the remains are removed from the primary chamber of the cremator. These remains are placed in urns and returned to the family for interment or disposal.



**Bl Cremation Systems, Inc.**

7205 - 114th Avenue North • Largo, Florida 33773  
 1-800-622-5411 • 727-541-4666 • Facsimile 727-547-0669  
 e-mail: blcremsys@aol.com • www.blcremationsystems.com

## PROCESS FLOW DIAGRAM



World's Largest Independent Cremation Equipment Manufacturer

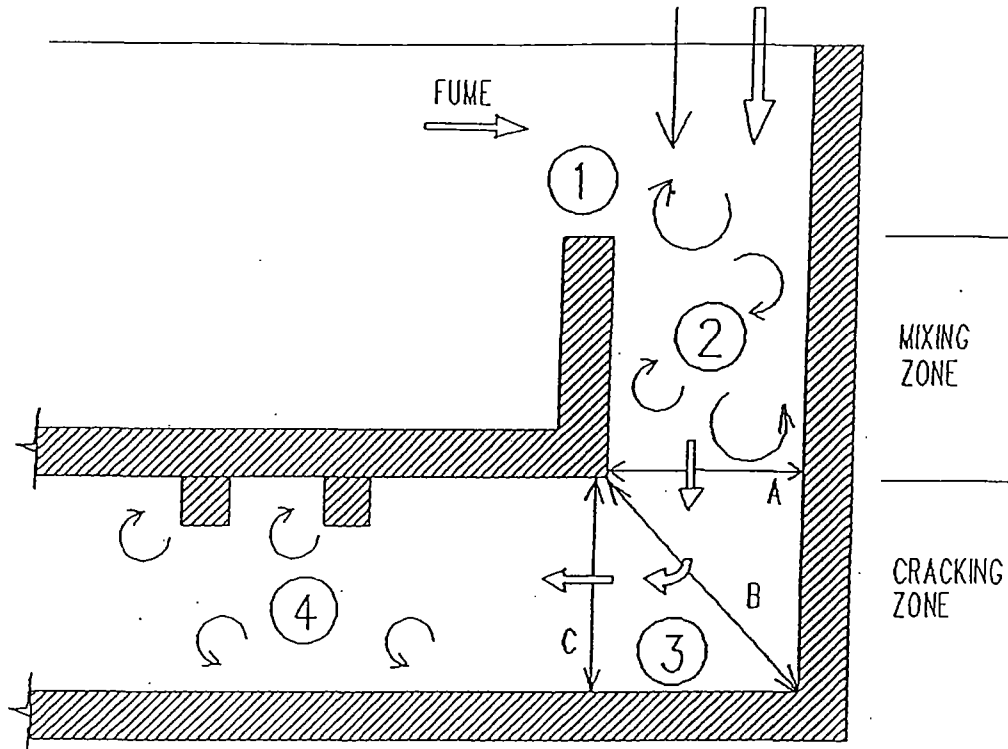




Cremation  
**Systems, Inc.**

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1-800-622-5411 • 727-541-4666 • Facsimile 727-547-0669

SECONDARY  
AIR BURNER



1. At the back of primary chamber, waste fume, air and burner flame all meet with different viscosities, volumes, velocities and flow directions which causes turbulence in the mixing zone of the secondary chamber.
2. Turbulence continues in the mixing zone as flows are traversing the flame tip.
3. Changing velocity at flame front zone and cornering cause additional turbulence at the base of the unit.  $V_A > V_B < V_C$ .
4. Uneven cross sectional area due to arches in the ceiling to support the primary chamber floor and additional changes in directional flow causes further turbulence downstream in the secondary chamber.

World's Largest Independent Cremation Equipment Manufacturer



Cremation  
**Systems, Inc.**

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1-800-622-5411 • 727-541-4666 • Facsimile 727-547-0669

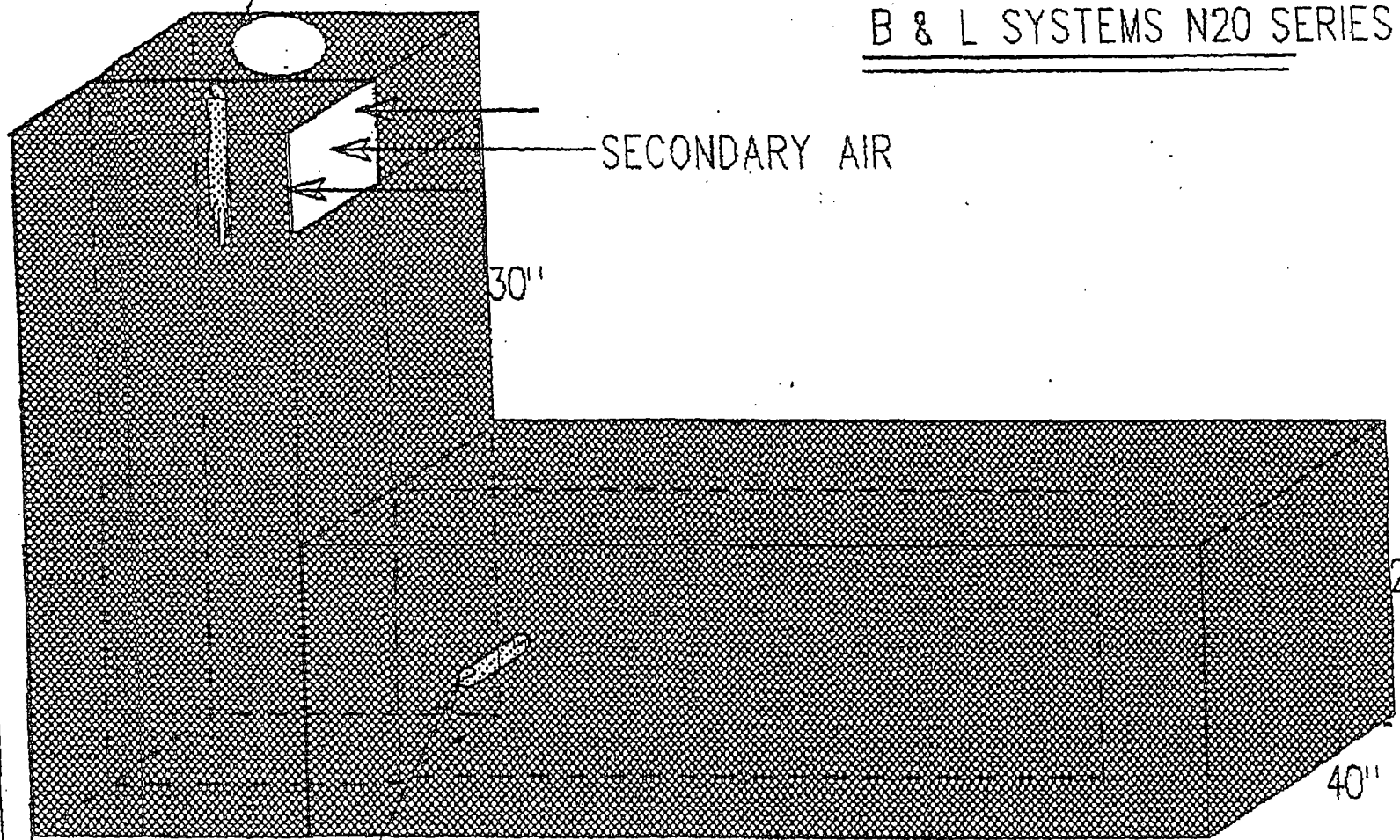
## TEMPERATURE CONTROL SEQUENCE

A type "K" thermocouple is placed 19<sup>3</sup> ft. down stream of the flame tip to measure temperature, the signal is sent to the *main control panel* where it is received by a FUJI PYZ series temperature controller with digital readout and a DR4200 *temperature recorder*. The FUJI PYZ series temperature controller controls the temperature via a *motorized butterfly valve* located on the *afterburner inlet gas assembly*. Gas demand is controlled by temperature to maintain a steady temperature. The *ignition/cremation burner* is interlocked to the *afterburning temperature* by the FUJI PYZ series temperature controller set point. Combustion cannot start until *temperature set point* is reached. Alarm contacts in the FUJI PYZ series temperature controller are utilized for over (high) temperature conditions. 100° F over set point the *afterburner* will be in maximum low fire and the *ignition/cremation burner* will shut off. The *butterfly valve* located on the *secondary air inlet* is controlled by a separate temperature out put to add air to cool the system. At *set point* the unit will return to normal operation. An optimonitor smoke detector is placed on the stack and set at 10% opacity if emissions occur the alarm will sound; a visual *red warning lamp* located on the *control panel* will illuminate and the *primary burners* will shut off. The *excess air butterfly valve* will open to add air to the *secondary chamber* to oxidize the emissions. After a five (5) minute period the unit will revert to normal operation.

B & L SYSTEMS N20 SERIES

AFTERBURNER

SECONDARY AIR



THERMOCOUPLE LOCATION  
20.0 FT

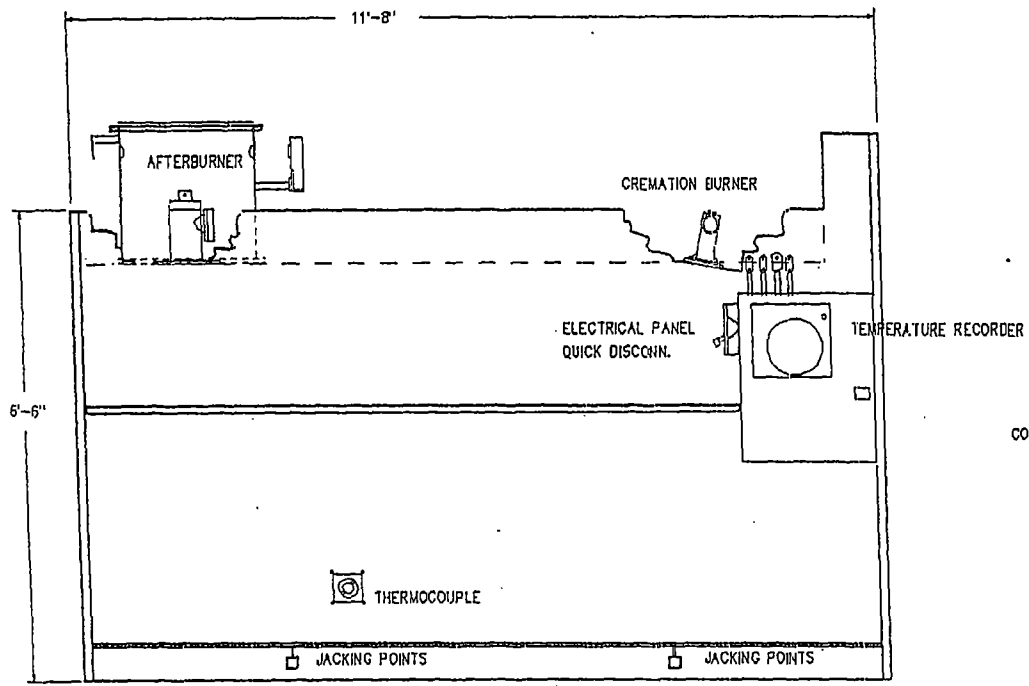
120"

30"

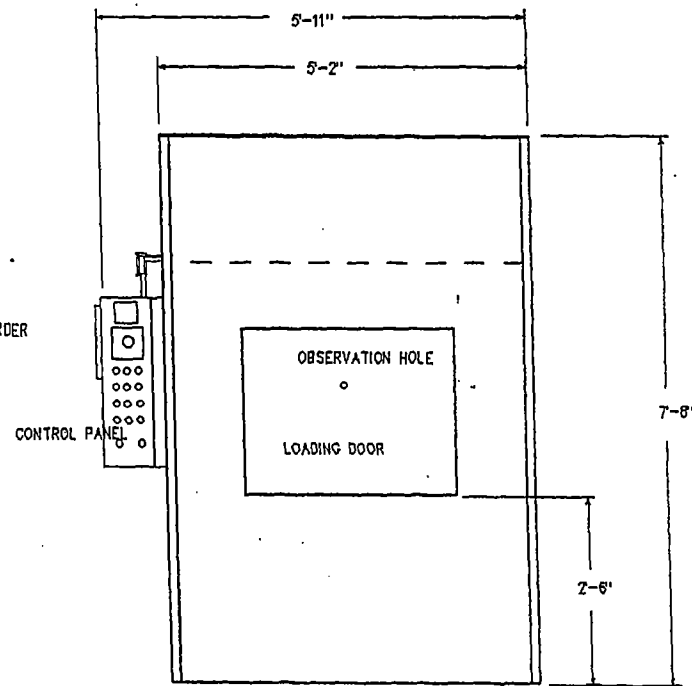
24"

40"

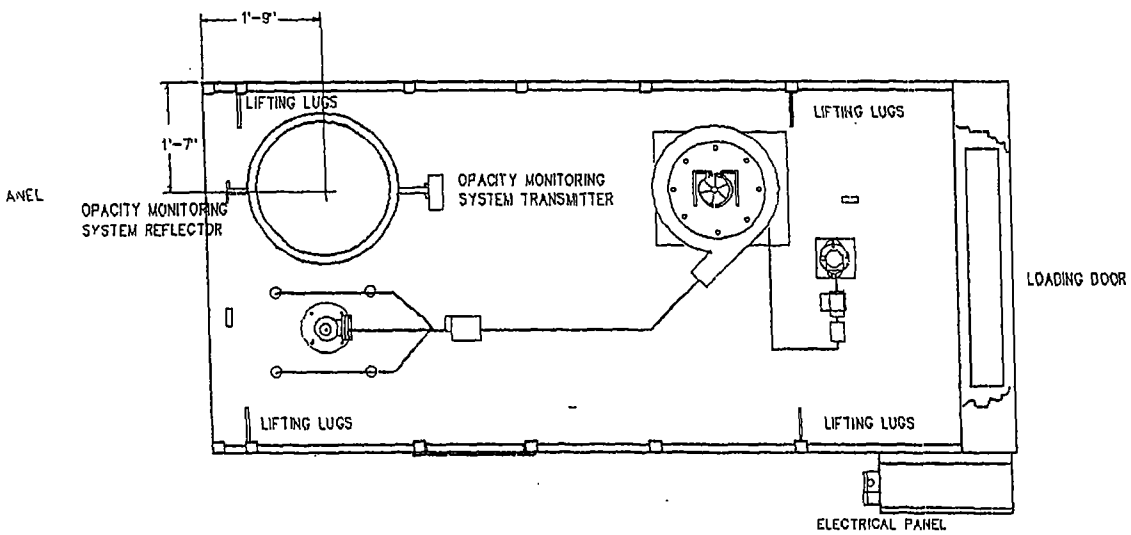
SHADED AREA REPRESENTS AFTERBURNER CHAMBER VOLUME OF  
83.00 FT<sup>3</sup> @ 1800 °F



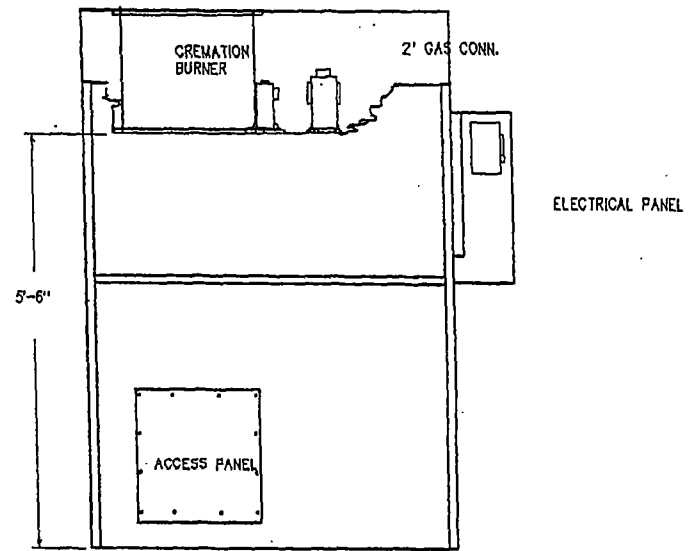
SIDE ELEVATION



FRONT ELEVATION



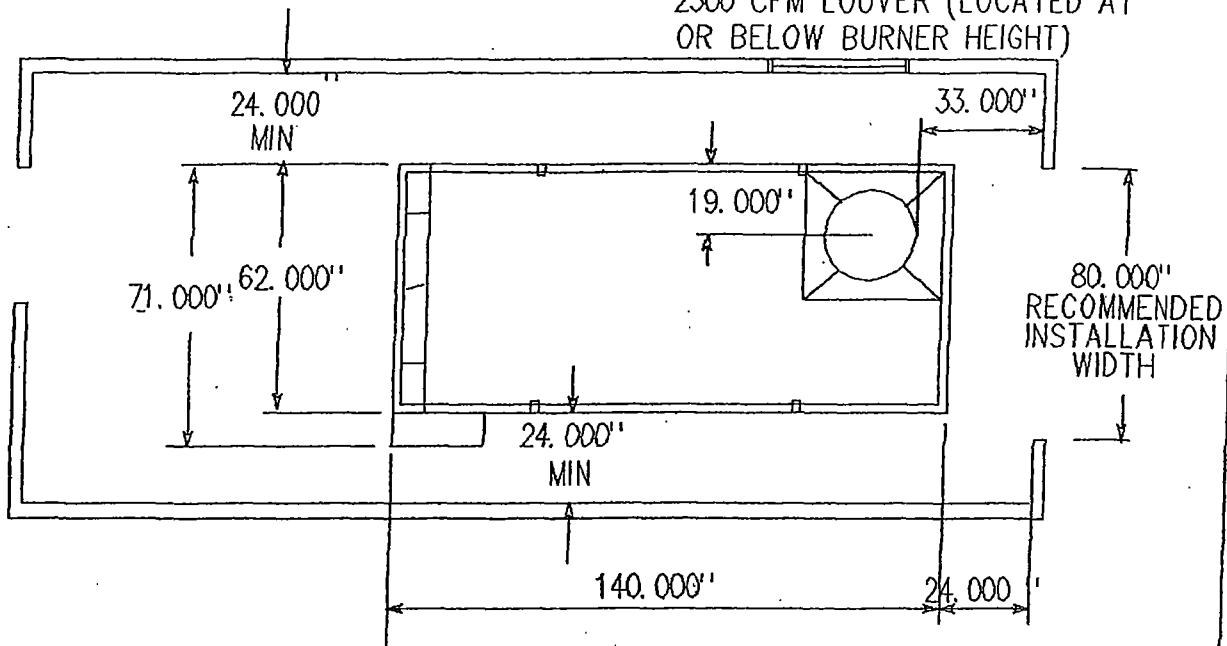
PLAN VIEW



N20SA REAR ELEVATION

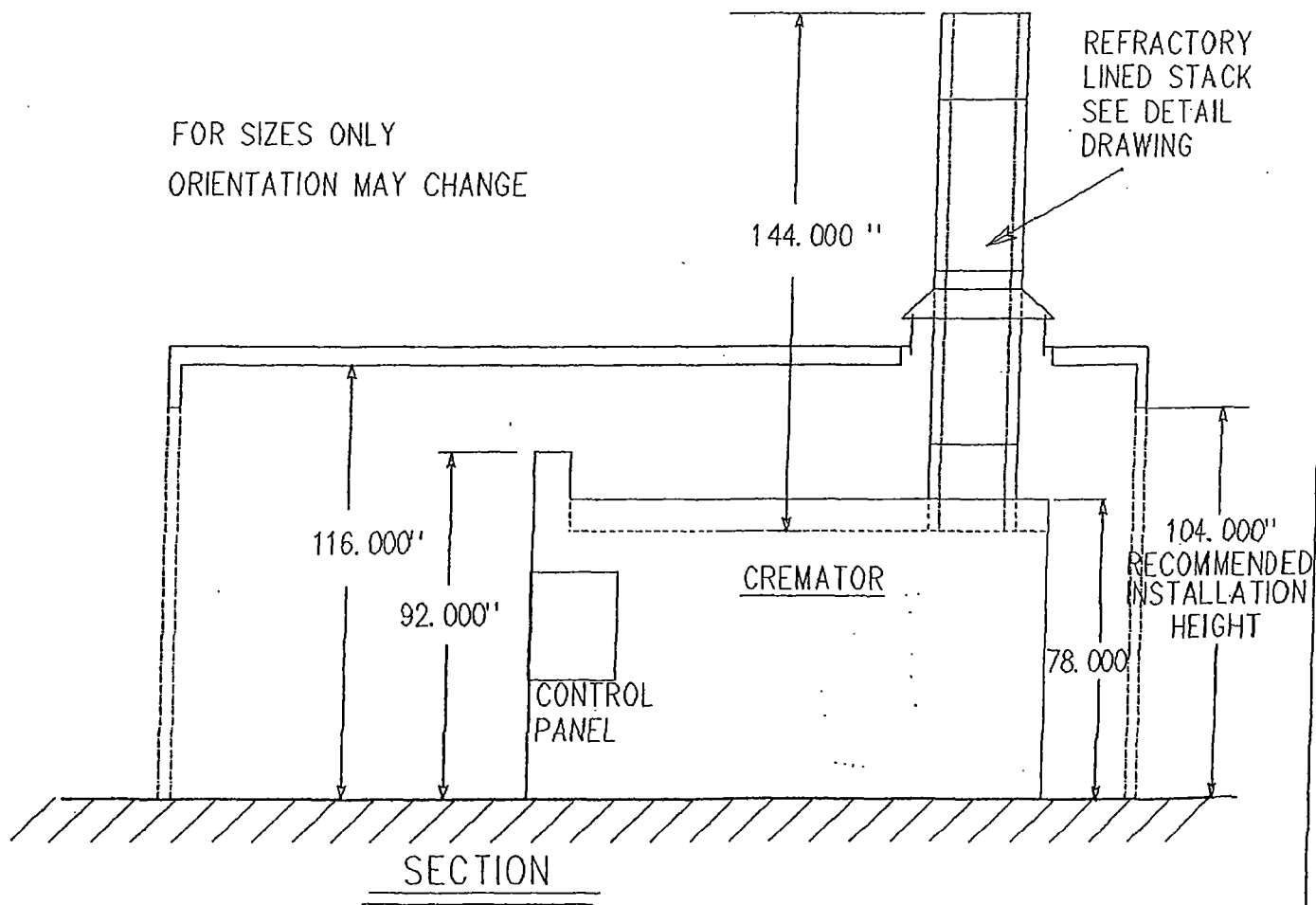
N20SA

2500 CFM LOUVER (LOCATED AT OR BELOW BURNER HEIGHT)



PLAN VIEW

FOR SIZES ONLY  
ORIENTATION MAY CHANGE



SECTION

Table 5.5-5  
ELEMENTAL CONTENT OF BODY FAT AND  
BODY WATER

Component	Mass (g)	Carbon Quantity* (g)	Hydrogen Quantity* (g)	Oxygen Quantity* (g)
Body fat	13,500	1.0E + 4	1.6E + 3	1.5E + 3
Essential	1,500	1.2E + 3	1.8E + 2	1.7E + 2
Nonessential	12,000	9.2E + 3	1.4E + 3	1.3E + 3
Body water	42,000		4.6E + 3	3.7E + 4
Extracellular	18,000		20.E + 3	1.6E + 4
Intracellular	24,000		2.6E + 3	2.1E + 4

\* For sources, see Reference 1.

From Snyder, W. S., Cook, M. J., Karhausen, L. R., Nasset, E. S., Howells, G. P., and Tipton, I. H., *Report of the Task Force on Reference Man*. ICRP Report No. 23, International Commission on Radiological Protection, Pergamon Press, Oxford, 1975, 1. With permission.

Table 5.5-6  
REFERENCE MAN: TOTAL BODY CONTENT FOR SOME ELEMENTS

Element	Amount (g)	Percent of total body weight	Element	Amount (g)	Percent of total body weight
Oxygen	43,000	61	Lead	0.12	0.00017
Carbon	16,000	23	Copper	0.072	0.00010
Hydrogen	7,000	10	Aluminum	0.061	0.00009
Nitrogen	1,800	2.6	Cadmium	0.050	0.00007
Calcium	1,000	1.4	Boron	<0.048	0.00007
Phosphorus	780	1.1	Barium	0.022	0.00003
Sulfur	140	0.20	Tin	<0.017	0.00002
Potassium	140	0.20	Manganese	0.012	0.00002
Sodium	100	0.14	Iodine	0.013	0.00002
Chlorine	95	0.12	Nickel	0.010	0.00001
Magnesium	19	0.027	Gold	<0.010	0.00001
Silicon	18	0.026	Molybdenum	<0.0093	0.00001
Iron	4.2	0.006	Chromium	<0.0018	0.000003
Fluorine	2.6	0.0037	Cesium	0.0015	0.000002
Zinc	2.3	0.0033	Cobalt	0.0015	0.000002
Rubidium	0.32	0.00046	Uranium	0.00009	0.0000001
Strontium	0.32	0.00046	Beryllium	0.000036	
Bromine	0.20	0.00029	Radium	$3.1 \times 10^{-11}$	

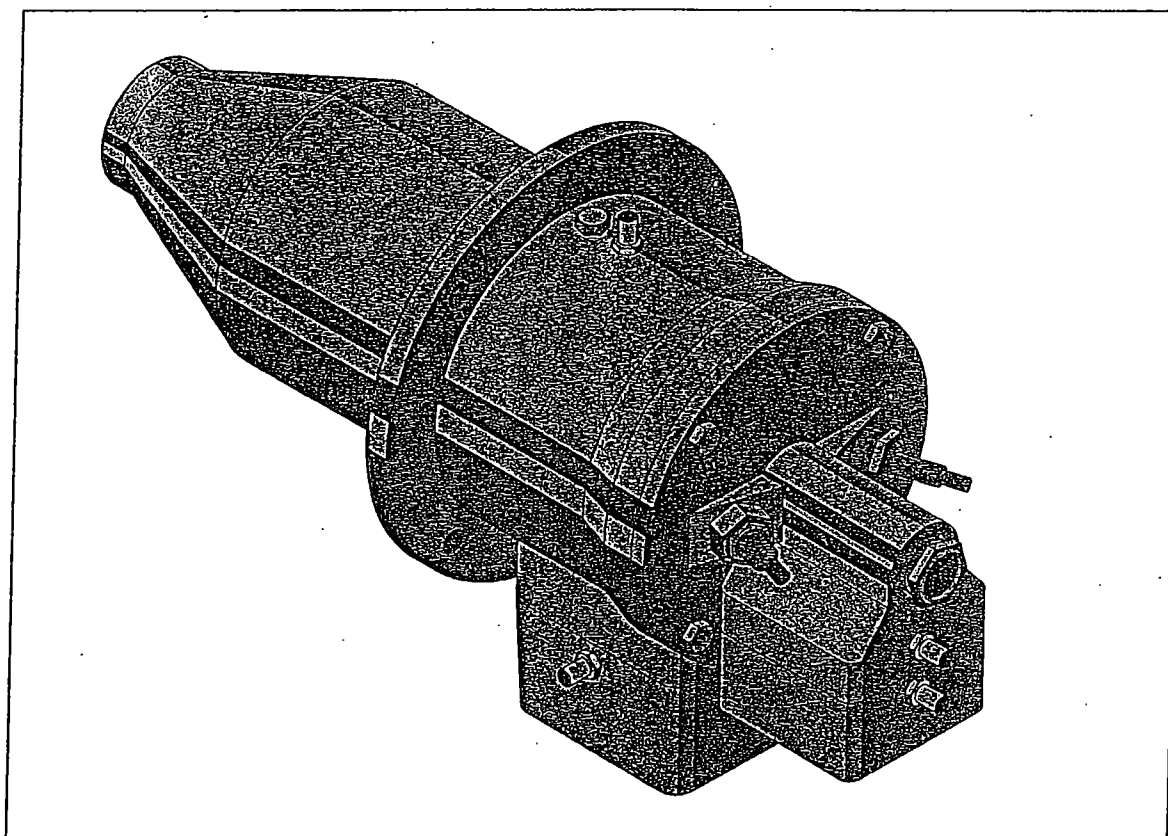
From Snyder, W. S., Cook, M. J., Karhausen, L. R., Nasset, E. S., Howells, G. P., and Tipton, I. H. *Report of the Task Group on Reference Man*, ICRP Report No. 23, International Commission on Radiological Protection, Pergamon Press, Oxford, 1975, 1. With permission.

**Instruction Manual**

No. 205, 11/95

# *Eclipse Velocity Burners*

*ThermJet Series (version 1.0)*



**Eclipse**

*Eclipse Combustion*

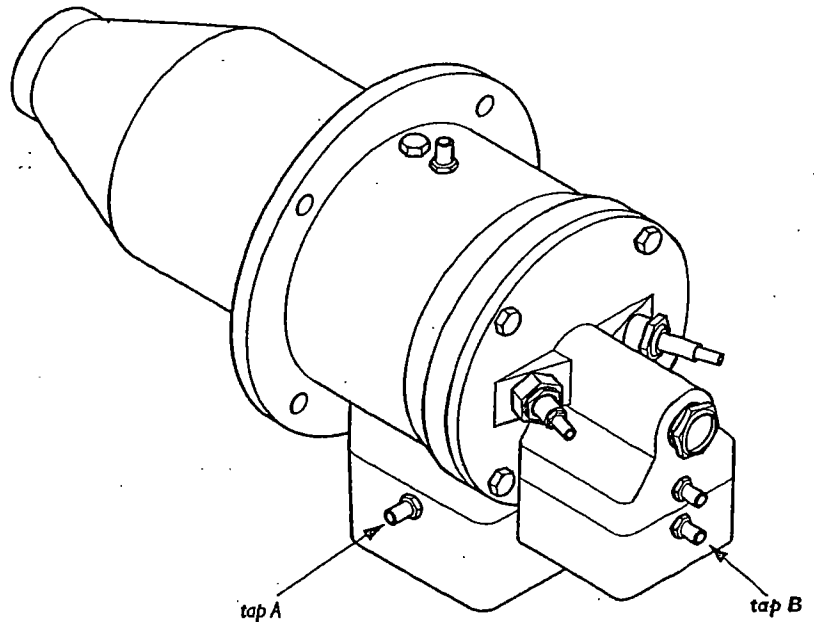
# Specifications

# 3

## INTRODUCTION

This section gives a detailed overview of the burner specifications. It also lists several options that are available for the ThermJet.

**Figure 3.1 The ThermJet burner**



**Table 3.1 Options**

PARAMETER	OPTIONS
Fuel	<ul style="list-style-type: none"> <li>• natural gas</li> <li>• propane</li> <li>• butane.</li> </ul> <p><i>For any other mixed gas, contact Eclipse for orifice sizing.</i></p>
Flame detection	<ul style="list-style-type: none"> <li>• U.V. scanner</li> <li>• flame rod, for use with alloy or silicon carbide firing tubes only.</li> </ul>
Ignition	<ul style="list-style-type: none"> <li>• direct spark ignition (6 kV AC).</li> </ul>
Combustor	<ul style="list-style-type: none"> <li>• alloy firing tube</li> <li>• silicon carbide firing tube</li> <li>• refractory block.</li> </ul>



# SPECIFICATIONS

## Main specifications

Table 3.2 Thermjet performance data

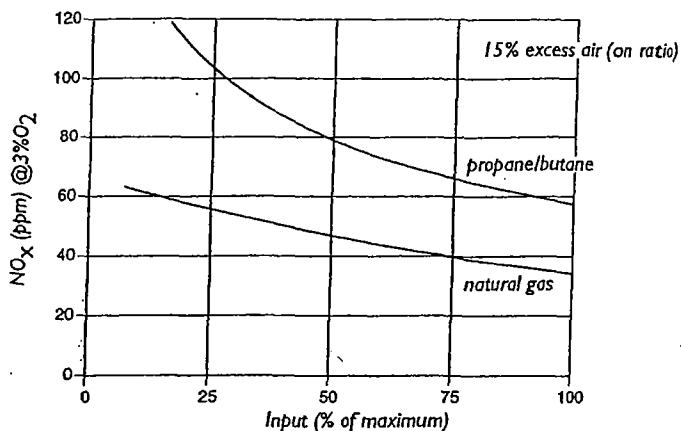
PARAMETER	BURNER TYPE (VELOCITY)	BURNER SIZE				
		50	75	100	150	
High fire input (Btu/hr)	Medium & High velocity	500,000	750,000	1,000,000	1,500,000	
Low firing rate, on-ratio (Btu/hr)	Medium & High velocity	50,000	75,000	100,000	150,000	
Low firing rate, fixed air (Btu/hr)	Medium & High velocity	10,000	15,000	20,000	30,000	
Static air pressure ("w.c.) • 15% excess air, at maximum input with standard orifice plate installed. measured at tap A (See Figure 3.1)	High velocity	12.0	16.0	14.5	18.5	
	Medium velocity	7.5	8.0	7.5	9.5	
Static gas pressure ("w.c.) • at maximum input with standard orifice plate installed. measured at tap B (See Figure 3.1)	High velocity	11.0	15.5	16.0	16.5	
	Medium velocity	6.0	6.5	7.5	8.0	
Flame length (In) (from end of firing tube)	High velocity	Nat. gas	25	30.4	33	38
		Propane	33	34	34	42
		Butane	30	30	35	43
	Medium velocity	Nat. gas	28	28	38	43
		Propane	36	38	37	42
		Butane	39	30	42	40
Maximum flame velocity (ft/s) • 15% excess air, at maximum input	High velocity	500	500	500	500	
	Medium velocity	250	250	250	250	

- all information is given for general sizing purposes only
- refer to data sheet for burner specific information
- all inputs based on gross calorific values

Performance graphs

The graphs that follow give you an approximate picture of the performance. Should you want more exact information, contact Eclipse Combustion.

Figure 3.2 NO<sub>x</sub> emissions

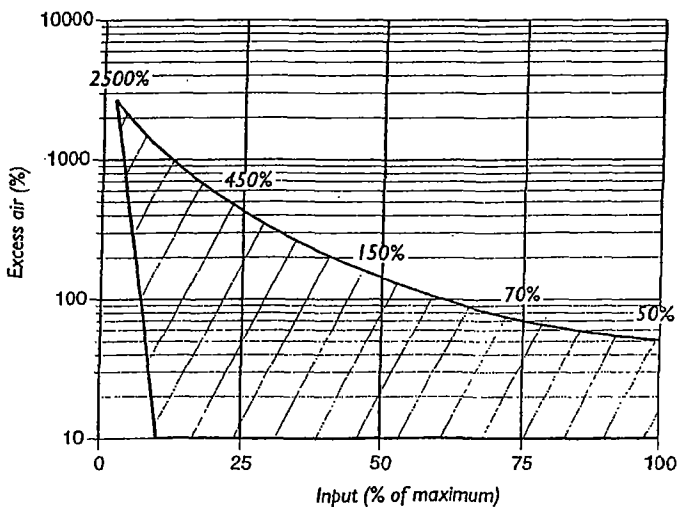


The emissions from the burner are influenced by:

- the fuel type
- the combustion air temperature
- the firing rate
- the chamber conditions
- the percent of excess air.

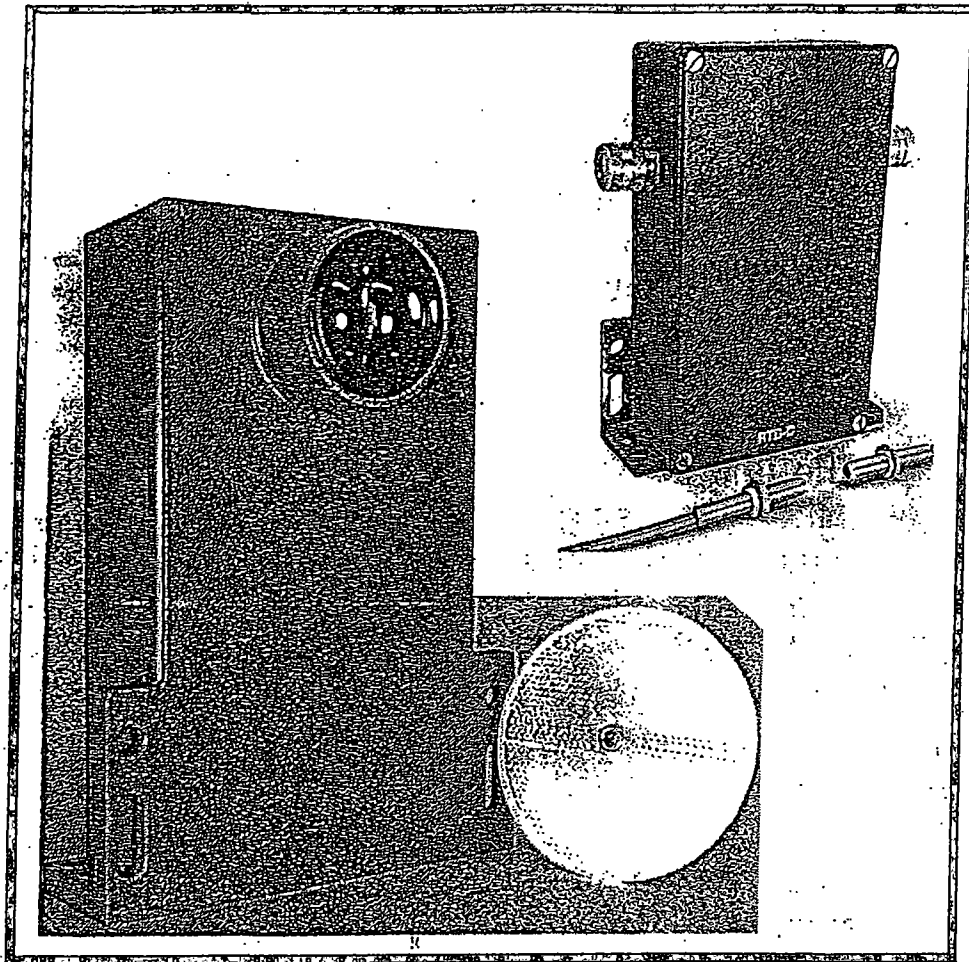
For estimates of other emissions, contact Eclipse Combustion.

Figure 3.3 Operational zone



OPTOMONITOR

## VISIBLE EMISSIONS ALARM (VEA)



**APPLICATION:** Alarm and control for Opacity used on small and large sources for warning operators and shutting down systems based on opacity, haze or clarity.

- Proven Rugged Design
- Unaffected by Ambient Light
- Spans up to 6 Feet
- Visible LED Light Source
- Dual Beam or Single Beam
- Adjustable Delay up to 3 min.
- Easy to Install & Support
- External Adjustment

# GENERAL PURPOSE OPACITY ALARMS



**APPLICATION:** These units are specifically designed to provide an operator with a reliable alarm system when Opacity or Smoke has exceeded a predefined limit. The alarm limit is easily set by using an opacity filter. The pulsed visible LED is unaffected by ambient light which makes for easy to install and calibrate.

**FEATURES:** The unit comes in either a single beam and dual beam design and an almost permanent LED light source. The electronics are housed in a rugged die-cast housing and powered by either 120 VAC or 230 VAC.

These designs meet all common installation requirements.

## SPECIFICATIONS:

**LIGHT SOURCE:** Pulsed Visible LED.  
**SPECTRAL RESPONSE:** Between 400nm & 500nm.  
**ANGLE OF VIEW:** Less than 4 degrees from axis.  
**AMBIENT LIGHT:** No measurable effect.

**RANGE:** 0 TO 100% Opacity.  
**ACCURACY:** +/- 3% of full scale.  
**ALARMS:** DPDT 5.0 A @ 120 VAC; 100% adj.  
LED Indicator for alarm setting.  
**OTHER OUTPUTS:** ON-OFF operation (no time delay).  
OFF time delay (reverse of normal).  
Adjustable One-shot.

**POWER:** 100-130 Volts AC, 50/60 Hz, 10 VA.  
**TEMPERATURE:** Ambient: -20 to +150 degrees F.  
Storage: +20 to +90 degrees F.  
**ENCLOSURES:** Meet NEMA 3,4,5,12.  
**PHYSICAL:** ELECTRONICS 8.0" x 5.75" x 3.31" (HWD).  
VEA-S SINGLE BEAM - 3/8"-24 inch. Straight Thread.  
VEA-D DUAL BEAM SENSOR - 3" Diameter.

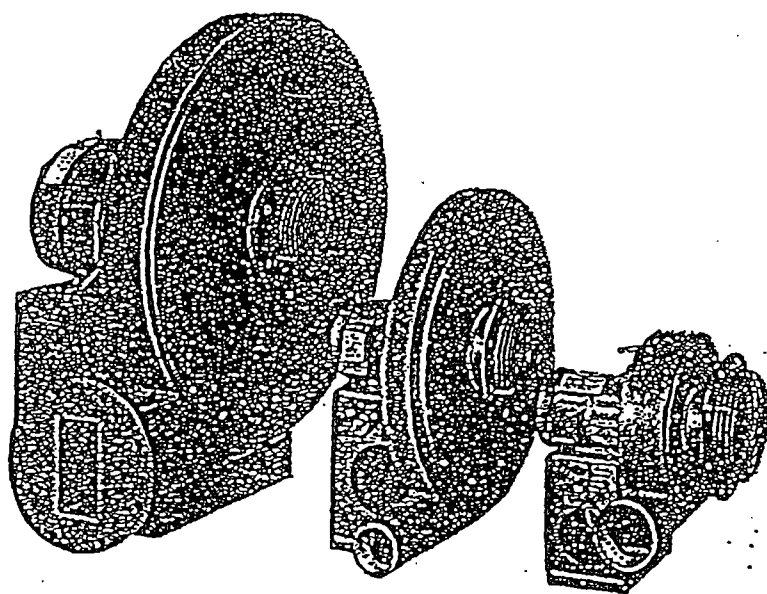
**RESPONSE TIME:** Selectable & Adjustable up to 3 minutes.

**OPTOMONITOR, Inc.**  
270 Polaris Avenue  
Mountain View, CA 94043  
Phone: 415/967-8992  
Fax: 415/967-0286

PLACE  
STAMP  
HERE

# ECLIPSE TURBO BLOWERS

## SERIES "SMJ"



- High efficiency
- Heavy gauge steel base and housing
- Aluminum impellers balanced statically and dynamically
- Matching air filters available
- Changeable outlet positions

Eclipse "SMJ" Blowers are centrifugal blowers that provide low pressure air for industrial combustion systems. They are also used for cooling, conveying, drying, liquid agitation, smoke abatement, vacuum cleaning, fume and dust exhausting, and other applications where air temperatures are under 220°F.

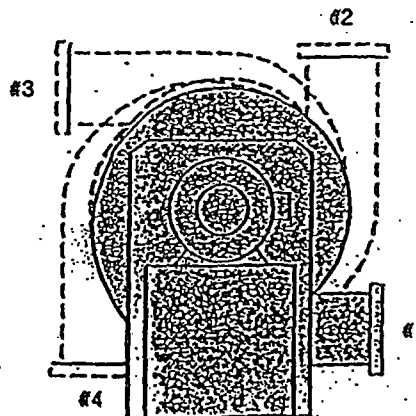
All "SMJ" Blowers are constructed of continuous welded, heavy gauge steel. The impellers are made of lightweight, high strength, riveted aluminum. Outlets on 3" and 4" models are threaded, while all others are flanged for a standard 125# ANSI companion flange. Discharge ports are sized to keep pressure losses within reasonable limits.

Blower inlet flanges are equipped with a grill that complies with OSHA regulations. If desired, the grill may be removed and the inlet bolted to a standard ANSI companion flange. Eclipse-supplied motors are standard shaft and starting torque, ball bearing, 3600 rpm units. On any blower requiring 3/4 HP or more, Eclipse recommends that polyphase motors be used.

There are four possible outlet positions. Any existing position is easily changed by removing the housing from the

blower base and remounting it in the desired position. Positions 1 through 3 can be specified for any blower. Position 4, however, requires factory approval before ordering. Position 1 is the standard assembly (bottom, horizontal) unless otherwise specified.

"SMJ" Blowers can be supplied with counterclockwise (CCW) or clockwise (CW) rotation as viewed from the motor side. CCW rotation is furnished standard unless otherwise specified.

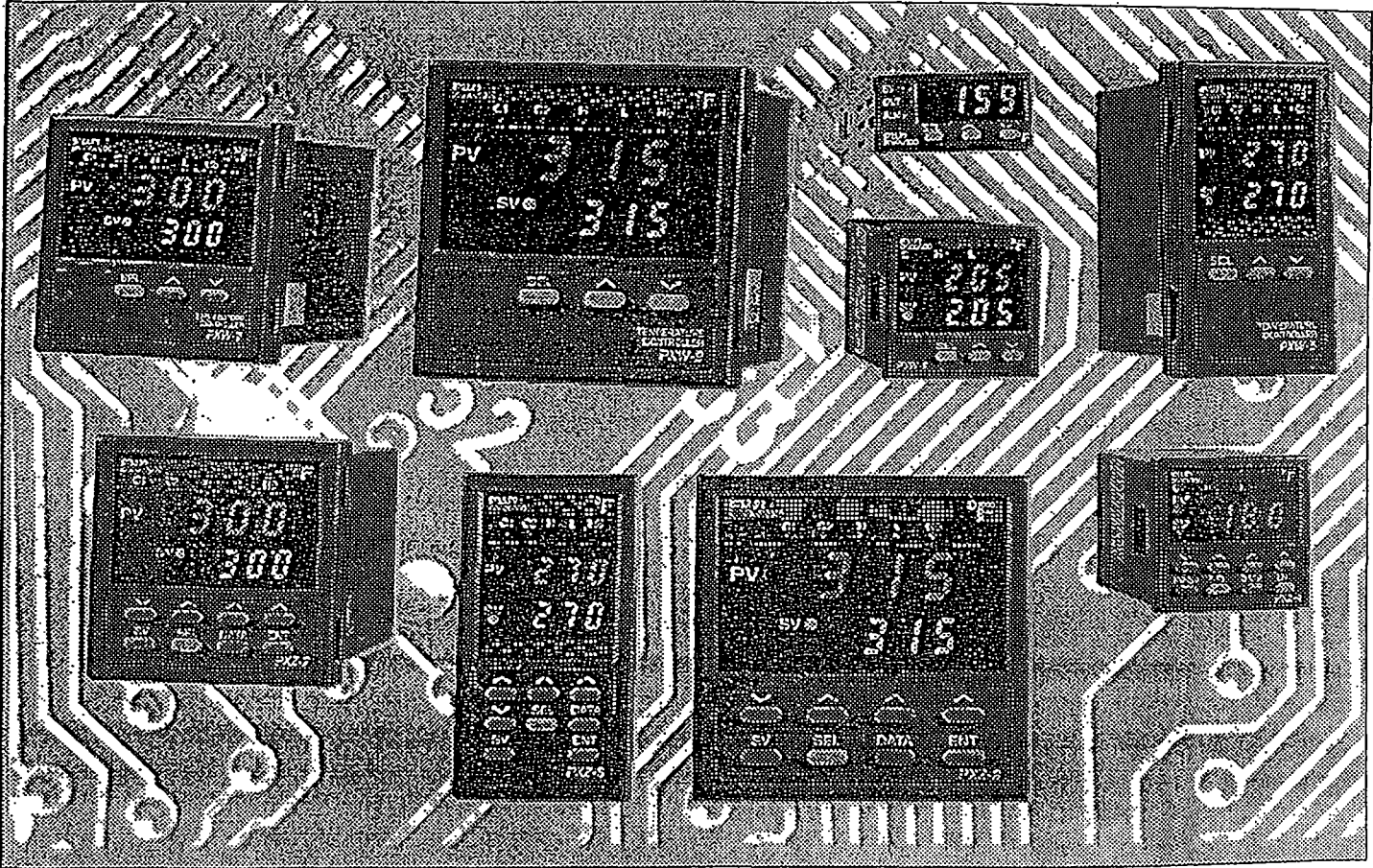


Outlet Positions

**FUJI**  
ELECTRIC

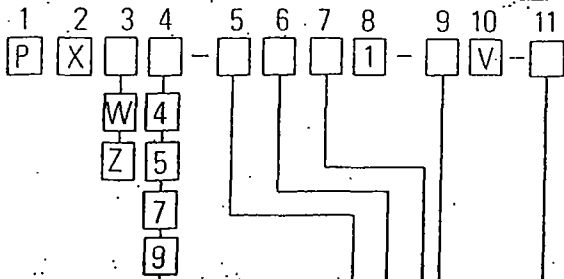
**PX SERIES**

PID Autotune  
Controllers  
Featuring Fuzzy Logic



Operation Manual

# MODEL CONFIGURATION



Front panel size	Code
48 x 48 (1/16 DIN)	4
48 x 96 (1/8 DIN)	5
72 x 72 (72mm)	7
96 x 96 (1/4 DIN)	9

Kinds of input	Code
Thermocouple (°C)	T
Thermocouple (°F)	R
RTD/Pt100 (°C)	N
RTD/Pt100 (°F)	S
4-20mA DC, 1-5V DC	B
0-20mA DC, 0-5V DC	A

Control output 1	Code
Relay contact (reverse action)	A
Relay contact (direct action)	B
SSR driver (reverse action)	C
SSR driver (direct action)	D
4 to 20mA DC (reverse action)	E
4 to 20mA DC (direct action)	F

Control output 2*	Code
None	Y
Relay contact (reverse action)	A
Relay contact (direct action)	B
SSR driver (reverse action)	C
SSR driver (direct action)	D
4 to 20mA DC (reverse action)	E
4 to 20mA DC (direct action)	F

\*not available on 48 x 48mm type

Additional function	Code
Heater break alarm*	2
Process alarm & Heater break alarm*	3
None	4
Process alarm	5

\*not available on 48 x 48mm type

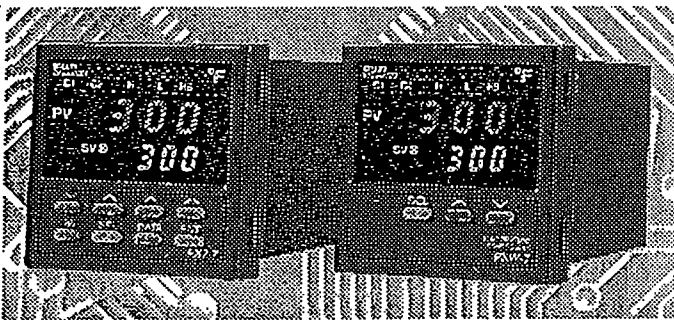
Power Supply Option	Code
24V AC/DC Supply	D

# FEATURES:

- 1/4 DIN, 1/8 DIN, 72mm, 1/16 DIN and 1/32 DIN sizes available
- Choose between 3-button or 8-button operation
- Fuzzy logic control with PID-Autotune
- Universal input-T/C, RTD, current, and voltage
- 24V DC/AC supply option available
- 8 segment ramp/soak programming
- Advanced security options to prevent unauthorized changes in parameters
- NEMA 4X faceplate

## GENERAL SPECIFICATIONS

Rated voltage	85-264V AC or 24 AC/DC
Power consumption	10VA or less (100V AC, without option) 15VA or less (220V AC, without option)
Insulation resistance	50M $\Omega$ or more (500V DC)
Withstand voltage	Power source-Earth: 1500V AC, 1 min Power source-Other: 1500V AC, 1 min Earth-relay output: 1500V AC, 1 min Earth-Alarm output: 1500V AC, 1 min Other: 500V AC, 1 min
Input impedance	Thermocouple: 1M $\Omega$ or more Voltage: 450K $\Omega$ or more Current: 250 $\Omega$ (external resistor)
Allowable signal source resistance	Thermocouple: 100 $\Omega$ or more Voltage: 1K $\Omega$ or more
Allowable wiring resistance	RTD: 10 $\Omega$ or less per wire
Reference junction compensation accuracy	$\pm 1.0^{\circ}\text{C}$ (at 23 $^{\circ}\text{C}$ )
Process variable offset	(PV shift) $\pm 10\%$ FS
Set variable offset	$\pm 50\%$ FS
Input filter	0-120.0 sec, setting in 0.1 sec steps (primary lagging filter)
Noise reduction ratio	Normal mode noise (50/60Hz): 50dB or more Common mode noise (50/60Hz): 140dB or more



PXZ and PXW 7

## POWER FAILURE PROCESSING

Memory protection:	Non-volatile memory hold After the recovery of power, control is started at the value before power failure
--------------------	---

## SELF-CHECK

Method:	Watchdog timer monitors program error.
---------	--

## OPERATION AND STORAGE CONDITIONS

Operating temperature	-10 to 50 $^{\circ}\text{C}$
Operating humidity	90% RH or less (non-condensing)
Storage temperature	-20 to 60 $^{\circ}\text{C}$

## CONTROL FUNCTION

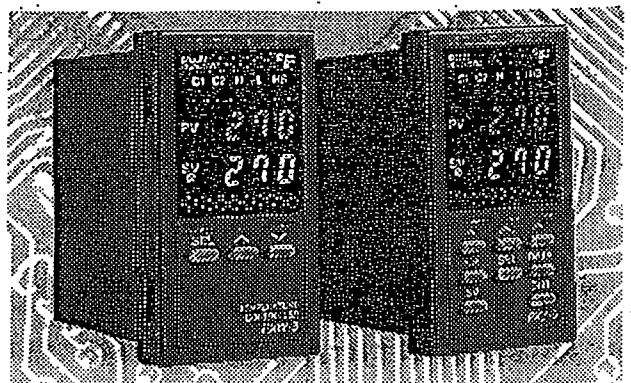
(STANDARD TYPE)

Control action	PID control with auto-tuning Fuzzy control with auto-tuning
Proportional band (P)	0-999.9%, setting in 0.1% steps
Integral time (I)	0-3200 sec, setting in 1 sec steps
Differential time (D)	0-999.9 sec, setting in 1 sec steps
P,I,D= 2-Pt. Position action when P,I,D=0 Proportional action when I,D=0	
Proportional cycle	1-150 sec, setting in 1 sec steps, relay contact output, SSR/SSC drive output only
Hysteresis width	0-50%, setting in 1% steps, 2-position action only
Anti-reset wind up	0-100% FS, setting in 1% steps, auto-setting with auto-tuning
Input sampling cycle	0.5 sec
Control cycle	0.5 sec

## CONTROL FUNCTION

(DUAL OUTPUT TYPE) (HEATING/COOLING TYPE)

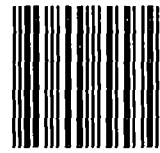
Heating Proportional band	P x 1/2 (P= 0-999.9%)
Cooling Proportional band	Heating proportional band x cooling proportional band coefficient Cooling proportional band coefficient= 0-99.9 0-2-position action
Integral time	0-3200 sec for heating and cooling
Differential time	0-999.9 sec for heating and cooling
P,I,D= 0-2-position action (without dead band) for heating and cooling I,D= 0:Proportional action	
Proportional cycle	1-150 sec, relay contact output, SSR/SSC drive output only
Hysteresis width	2-position action for heating and cooling: 0.5% FS 2-position action for cooling: 0.5% FS
Anti-reset wind-up	0-100% FS, setting in 1% steps, auto setting with auto-tuning
Overlap/dead band	$\pm 50\%$ of heating proportional band
Input sampling cycle	0.5 sec
Control cycle	0.5 sec



PXW and PXZ 5



OB 668  
7FS, FL 32435-0668



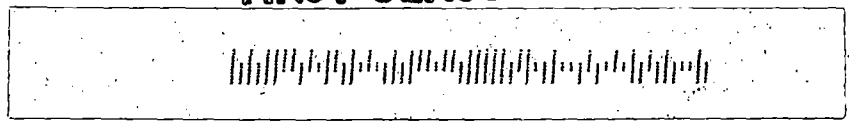
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