## RECEIVED

## ANIMAL CREMATORY AIR GENERAL PERMIT REGISTRATION FORM

DEC 1 - 2010

Part II. Notification to Permitting Office

Bureau of Air Monitoring

(Detach and submit to appropriate permitting office; keep copy onsite), Mobile Sources

Instructions: To give notice to the Department of an eligible facility's intent to use this air general permit, the owner or operator of the facility must detach and complete this part of the Air General Permit Registration Form and submit it to the appropriate Department of Environmental Protection or local air pollution control program office which has permitting authority. Please type or print clearly all information, and enclose the appropriate air general permit registration processing fee pursuant to Rule 62-4.050, F.A.C. (\$100 as of the effective date of this form)

Registration Type	0/3	0043-00
Check one:		
INITIAL REGISTRATION - Notificati Construct and operate a proposed new Operate an existing facility not currer air operation permit to an air general	w facility. ntly using an air general permit (e.g	., a facility proposing to go from an
RE-REGISTRATION (for facilities curred)  Continue operating the facility after a Continue operating the facility after a Make an equipment change requiring other change not considered an administration.	expiration of the current term of air a change of ownership.  gre-registration pursuant to Rule 62.	general permit use210.310(2)(e), F.A.C., or any
Surrender of Existing Air Operation Per	mit(s) - For Initial Registrations (	Only
If the facility currently holds one or more a or operator upon the effective date of this a operation permits being surrendered. If no  All existing air operation permits for general permit; specifically permit no	ir general permit. In such case, che air operation permits are held by the this facility are hereby surrendered	ck the first box, and indicate the e facility, check the second box.
No air operation permits currently ex	ist for this facility.	
General Facility Information Facility Owner/Company Name (Name of coperates, controls, or supervises the facility Pet Haven Cemetery & Crematory	) NOTE: STILL NORTH	
Site Name (Name, if any, of the facility site owned, a registration form must be complet Pet Haven Cemetery & Crematory		c. If more than one facility is
Facility Location (Provide the physical local Street Address: 27200 Jones Loop Rd	ation of the facility, not necessarily t	the mailing address.)
City:Punta Gorda	County:Charlotte	Zip Code:33982 <b>-2384</b>
	· · · ·	

DEP Form No. 62-210.920(2)(d) Effective: January 10, 2007 Facility Start-Up Date (Estimated start-up date of proposed new facility.) (N/A for existing facilities) Jan 2011

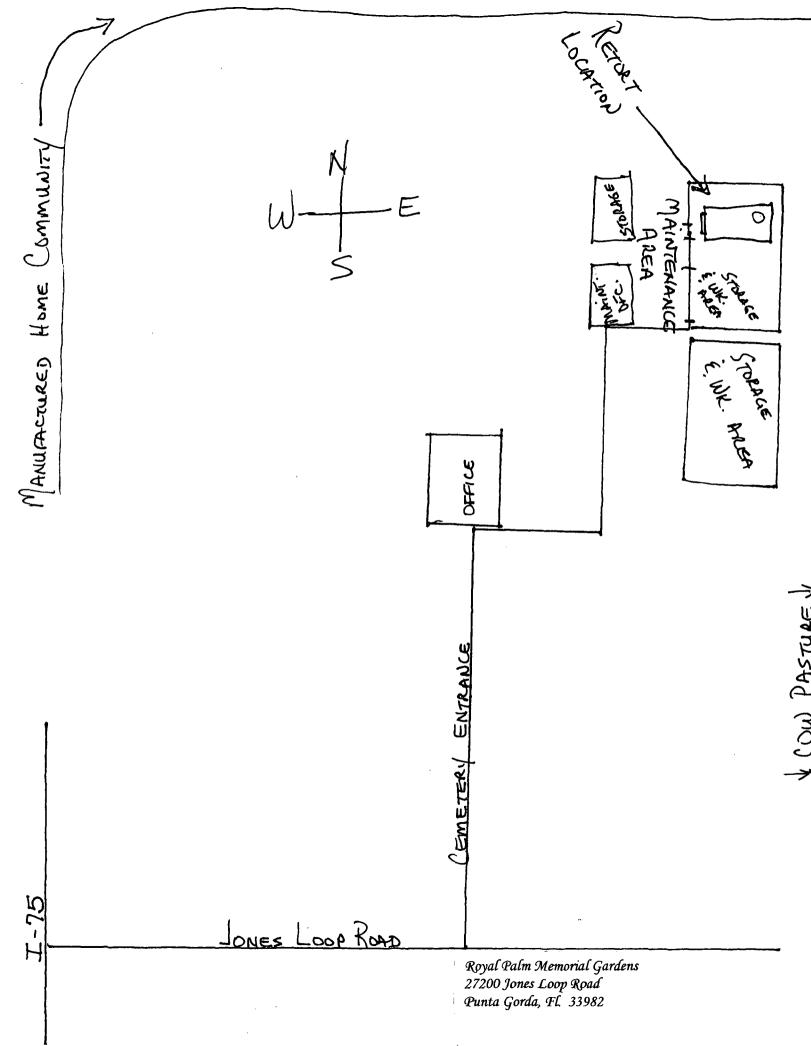
1000

DEP Form No. 62-210.920(2)(d) Effective: January 10, 2007

Owner/Authorized Representation Name and Position Title; (Person		ifies that the facility is eligible to use this
air general permit.)	·, ·, · · · · · · · · · · · · · · · · ·	, <del></del>
Print Name and Title: Karen Mo	onnier GM	
Owner/Authorized Representative	_	
Organization/Firm:Pet Haven C	emetery & Crematory	
Street Address: 27200 Jones Lo	op:Rd:	· · · · · · · · · · · · · · · · · · ·
City:Punta Gorda	County: Charlotte	Zip Code:33982
Owner/Authorized Representative	Telephone Numbers	
Telephone:941-639-2381	Fax:	
Cell phone (optional):		
Facility Contact Of different force	Oww.s/Assthaniand Damesantativ	
	m Owner/Authorized Representative pages or person to be contacted regard	ding day-to-day operations at the facility.
Print Name and Title:Karen Mor		ding day-to-day operations at the facility.
Time Name and Thie Real Cit 19101	mici Givi	
Facility Contact Mailing Address		
Organization/Firm:		
Street Address:		
City:	County:	Zip Code:
Facility Contact Telephone Number	arc	
Telephone:	Fax:	
Cell phone (optional):	T u.v.	
· · · · · · · · · · · · · · · · · · ·		
Owner/Authorized Representati		
_	dated by the person named above as	<del>-</del>
	ner or authorized representative of the	
	Permit Registration Form. I hereby o	
	inquiry, that the facility addressed in	
	and that the statements made in this re	•
		described in this registration form so
	le standards for control of air polluta	
the State of Florida and rules	of the Department of Environmental I	Protection and revisions thereof.
I will promptly notify the Den	artment of any changes to the informa	tion contained in this registration
form.	in incinio, any changes to the informa	mon commune in this registration
		$\mathcal{O}$
$\nu$ $\sim$ $\sim$ $\sim$ $\sim$		<b>γ</b> ]

DEP Form No. 62-210.920(2)(d) Effective: January 10, 2007

Design Calculations
If this is an initial registration for a proposed new animal crematory unit, provide design calculations to confirm a sufficient volume in the secondary chamber combustion zone to provide for at least a 1.0 second gas residence time at 1800 degrees F.
Manufacturer's' design calculations attached.
Registration is not for proposed new animal crematory unit(s).
Description of Facility
Below, or as an attachment to this form, provide a description of all crematory operations at the facility in sufficient detail to demonstrate the facility's eligibility for use of this air general permit and to provide a basis for tracking any future equipment or process changes at the facility. Describe all air pollutant-emitting processes and equipment at the facility, and identify any air pollution control measures or equipment used. Removal of existing Crawford C-1000 Pet Crematory & installation of a B&L Cremation Systems Inc Pet Crematory Model BLP 500
·
·
·



#### CALCULATIONS FOR PRODUCTS OF COMBUSTION AND RESIDENCE TIME FOR 150 LB/hr TYPE IV WASTE. B&L ANIMAL CREMATORY

#### **PROPANE**

#### A. BASIS: 1 LB WASTE

1. <u>1 lb waste X 1000 Btii/lb waste X 15 lbs air</u> = 1.5 lbs air 10,000 Btu

2. 1 lb waste  $\times$  0.10 lb combustible = 0.10 lbs of combustibles

1 lb waste

3. 1 lb waste X 0.85 lb H20 X 1.6\* = 1.36 lbs of water

1 lb waste

4.  $\underline{6,500 \text{ Btu aux fuel**} \text{ X 23.8 cu ft air/cu ft fuel}}$  = 4.64 lbs of air for aux fuel

2500 Btu/cu ft fuel X 13.35 cu ft air/lb air @ 70f

5.  $\underline{6,500 \text{ Btu aux fuel X 0.044 lb fuel/cu ft fuel}}$  = 0.11 lb of aux fuel

2500 Btu/cu ft fuel

6. Sum = PRODUCTS OF COMBUSTION (POC) = 7.71 lbs POC per lb

waste @ 70f

#### B. RESIDENCE TIME @ 1600 F

1. <u>7.71 lbs POC/lbs waste X 51.89 cu ft / lb POC @ 1600f X 150 lbs waste / hr</u> 3600 sec/hr

= 16.66 cu ft / sec @ 1600 f = 17.00 cu ft for 1 second residence time

#### RESIDENCE TIME @ 1800 F

- 2. <u>7.71 lbs POC/lbs waste X 56.93 cu ft /lb POC @ 1800f X 150 lbs waste / hr</u> 3600 sec/hr
  - = 18.28 cu ft / sec @ 1800f = 19.00 cu ft for 1 second residence time
- \* Correction multiplier for dry air and water vapor
- \*\* Fuel is propane

Referances: Incinerator institute of America.

North American Combustion Handbook Eclipse Combustion Engineering guide

#### C. THERMOCOUPLE PLACEMENT.

Secondary chamber operating temperature at > or = to 1600f = 17.00 cu ft from flame tip. 1800f = 19.00 cu ft from flame tip.



7205 - 114th Avenue North • Largo, Florida 33773 1-800-622-5411 • 727-541-4666 • Facsimile 727-547-0669 e-mail: blcremsys@aol.com • www.blcremationsystems.com

### PROCESS DESCRIPTION

This project consists of the construction of one new cremation retort. This crematorium will consist of one B & L Systems Model BLP 500/150 Animal Cremator. The cremation unit will be fired on propane.

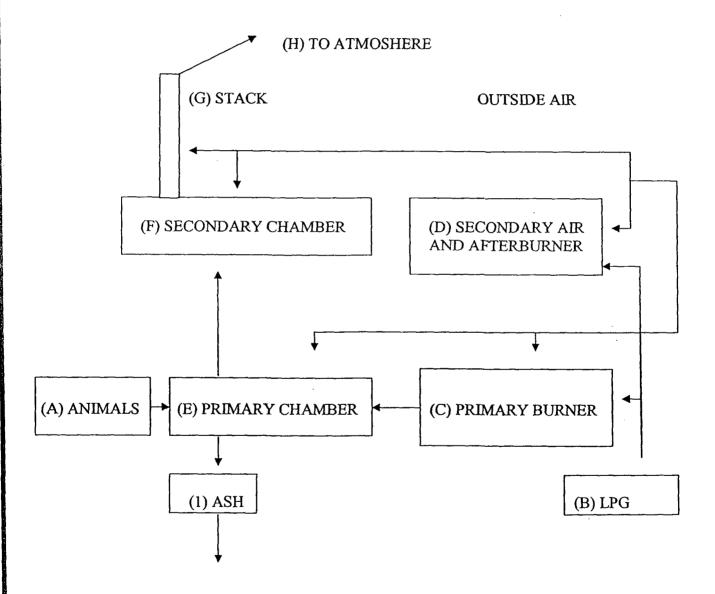
Deceased animal remains are manually placed into the primary chamber of the cremator. The door of the cremator is then closed. After a preheat of the afterburning chambers by the auxiliary burner, initial and supplementary combustion is provided by propane fired burner located in the primary chamber of the cremator. Once material combustion is initiated, the rate of the combustion is controlled by limiting both the combustion air and fuel supplied to the primary chamber through the primary burner. This process generates a highly combustible gas mixture that flows into a secondary chamber where more air is admitted to insure further oxidation of the gases. The auxiliary burner is installed in the secondary chamber of the cremator to facilitate complete combustion of all gaseous materials entering this chamber.

Once the cremation process is complete, the remains are removed from the primary chamber of the cremator. These remains are placed in urns and returned to the family for interment of disposal.



7205 - 114th Avenue North • Largo, Florida 33773 1-800-622-5411 • 727-541-4666 • Facsimile 727-547-0669 e-mail: blcremsys@aol.com • www.blcremationsystems.com

## PROCESS FLOW DIAGRAM



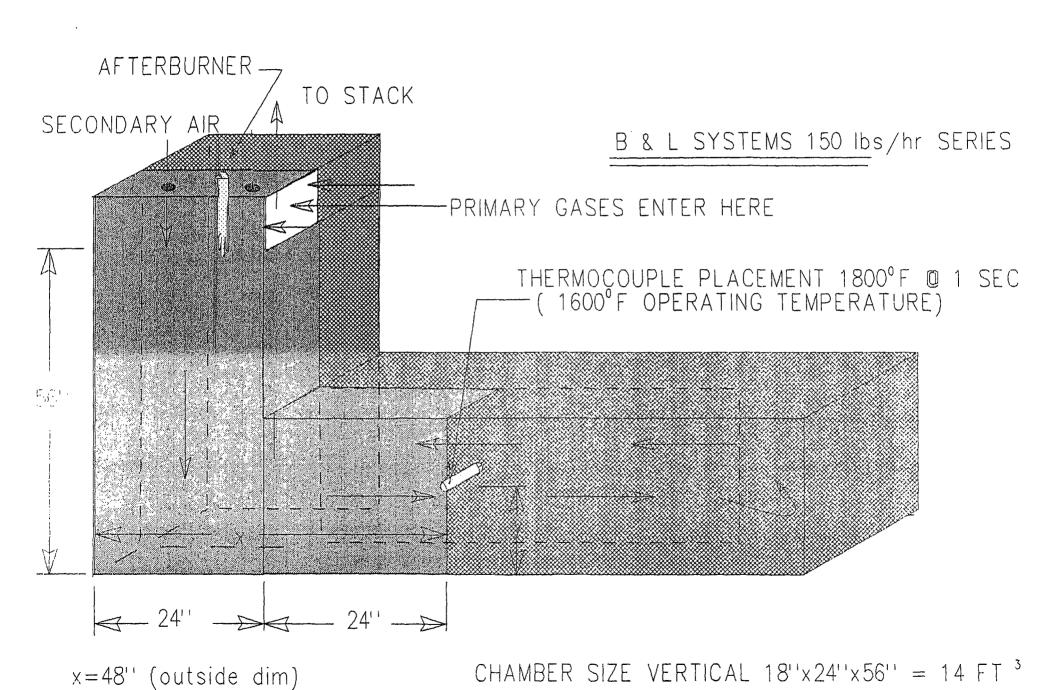
World's Largest Independent Cremation Equipment Manufacturer



7205 - 114th Avenue North • Largo, Florida 33773 1-800-622-5411 • 727-541-4666 • Facsimile 727-547-0669 e-mail: blcremsys@aol.com • www.blcremationsystems.com

#### TEMPERATURE CONTROL SEQUENCE

A type "K" thermocouple is placed 19 ft. down stream of the flame tip to measure temperature, the signal is sent to the main control panel where it is received by a FUJI PYZ series temperature controller with digital readout and a DR4200 temperature recorder. The FUJI PYZ series temperature controller controls the temperature via a motorized butterfly valve located on the afterburner inlet gas assembly. Gas demand is controlled by temperature to maintain a steady temperature. The ignition/cremation burner is interlocked to the afterburning temperature by the FUJI PYZ series temperature controller set point. Combustion cannot start until temperature set point is reached. Alarm contacts in the FUJI PYZ series temperature controller are utilized for over (high) temperature conditions. 100° F over set point the afterburner will be in maximum low fire and the ignition/cremation burner will shut off. The butterfly valve located on the secondary air inlet is controlled by a separate temperature out put to add air to cool the system. At set point the unit will return to normal operation. An optimonitor smoke detector is placed on the stack and set at 10% opacity if emissions occur the alarm will sound; a visual red warning lamp located on the control panel will illuminate and the primary burners will shut off. The excess air butterfly valve will open to add air to the secondary chamber to oxidize the emissions. After a five (5) minute period the unit will revert to normal operation.



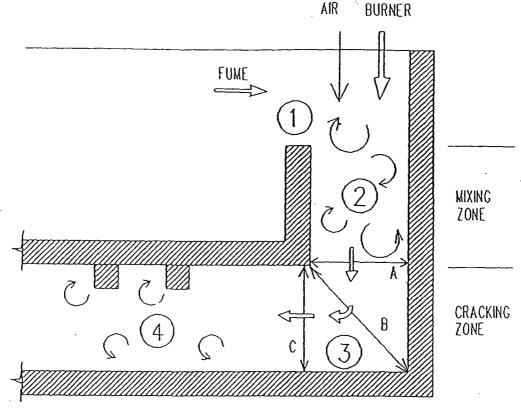
y=11.5''(outside dim)

HORIZONTAL  $18'' \times 20'' \times 24'' = 05 \text{ FT}^3$ 

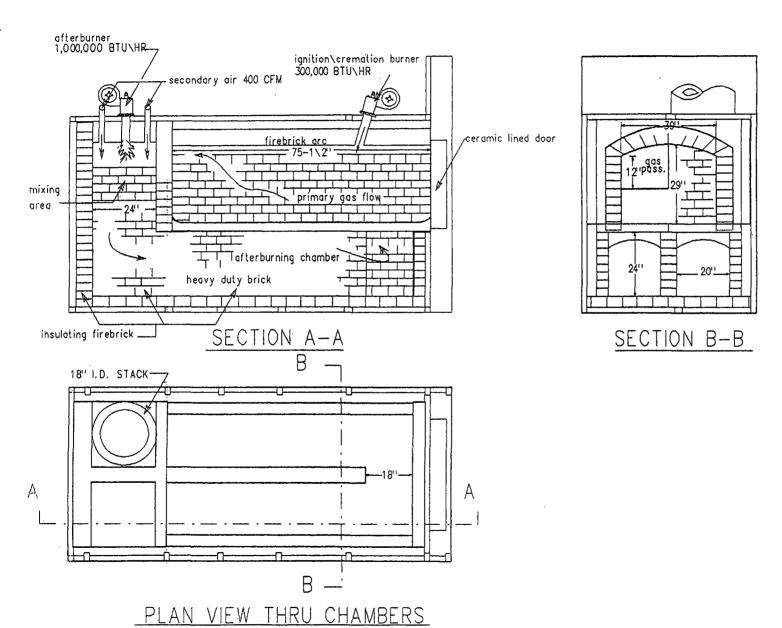


7205 - 114th Avenue North • Largo, Florida 33773 1-800-622-5411 • 727-541-4666 • Facsimile 727-547-0669

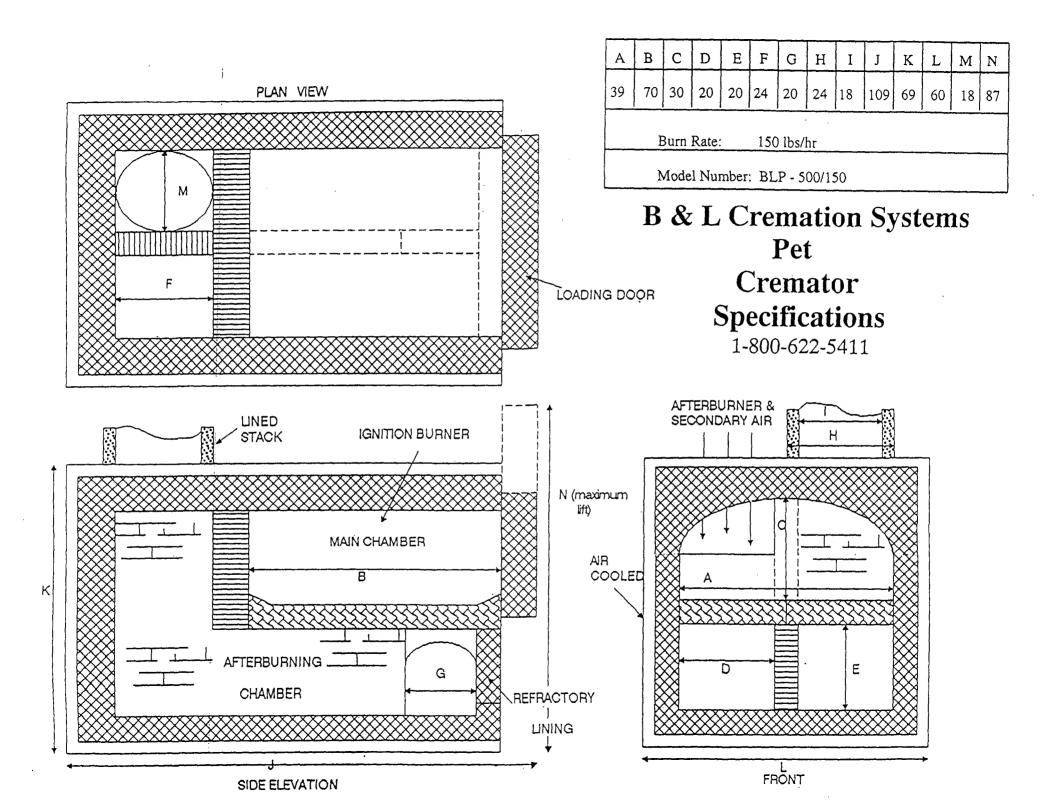
SECONDARY



- 1. At the back of primary chamber, waste fume, air and burner flame all meet with different viscosities, volumes, velocities and flow directions which causes turbulence in the mixing zone of the secondary chamber.
- 2. Turbulence continues in the mixing zone as flows are traversing the flame tip.
- 3. Changing velocity at flame front zone and cornering cause additional turbulence at the base of the unit.  $V_A > V_B < V_C$ .
- 4. Uneven cross sectional area due to arches in the ceiling to support the primary chamber floor and additional changes in directional flow causes further turbulence downstream in the secondary chamber.



BLP 500\150 ANIMAL CREMATOR

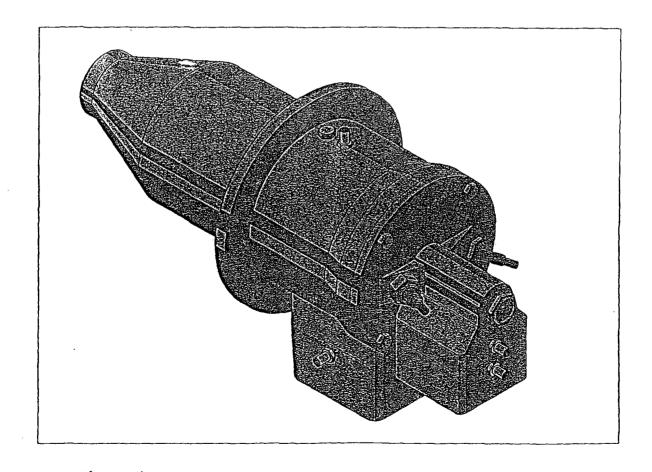




No. 205, 11/95

## Eclipse Velocity Burners

Therm Jet Series (version 1.0)



Eclipse Combustion



#### INTRODUCTION

This section gives a detailed overview of the burner specifications. It also lists several options that are available for the ThermJet.

Figure 3.1 The ThermJet burner

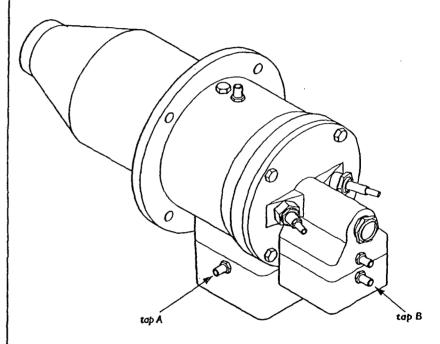


Table 3.1 Options

PARAMETER Fuel	<ul><li>natural gas</li><li>propane</li></ul>	For any other mixed gas, contact Eclipse for orifice sizing.
Flame detection	<ul><li>butane.</li><li>U.V. scanner</li><li>flame rod, for use with alloy or s</li></ul>	silicon carbide firing tubes only.
<b>Ignition</b>	<ul> <li>direct spark ignition (6 kV AC).</li> </ul>	
Combustor	<ul><li>alloy firing tube</li><li>silicon carbide firing tube</li><li>refractory block.</li></ul>	

#### **SPECIFICATIONS**

#### Main specifications

Table 3.2 ThermJet performance data

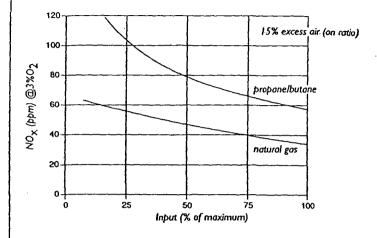
PARAMETER	BÜRNER I			BURNI	RSIZE .	
	(VELOGI	(Y)	50	75	100	150
High fire input (Btu/hr)	Medium & High ve	elocity	500,000	750,000	1,000,00 0	1,500,00
Low firing rate, on-ratio (Btu/hr)	Medium & High ve	locity	50,000	75,000	100,000	150,000
Low firing rate, fixed air (Btu/hr)	Medium & High ve	locity	10,000	15,000	20,000	30,000
Static air pressure ("w.c.)	High velocity		12.0	16.0	14.5	18.5
<ul> <li>15% excess air, at maximum input with standard orifice plate installed. measured at tap A (See Figure 3.1)</li> </ul>	Medium velocity		7.5	8.0	7.5	9.5
Static gas pressure ("w.c.)	High velocity		11.0	15.5	16.0	16.5
• at maximum input with standard orifice plate installed. measured at tap B (See Figure 3.1)	Medium velocity		6.0	6.5	7.5	8.0
Flame length (In) (from end of firing tube)	High velocity	Nat. gas	25	30.4	33	38
		Propane	33	34	34	42
		Butane	30	30	35	43
	Medium velocity Nat. gas Propane Butane	Nat. gas	28	28	38	43
		Propane	36	38	37	42
		39	30	42	40	
Maximum flame velocity (ft/s)	High velocity		500	500	500	500
15% excess air, at maximum input	Medium velocity		250	250	250	250

- all information is given for general sizing purposes only
- refer to data sheet for burner specific information
- · all inputs based on gross calorific values

#### Performance graphs

The graphs that follow give you an approximate picture of the performance. Should you want more exact information, contact Eclipse Combustion.

Figure 3.2 NO<sub>x</sub> emissions

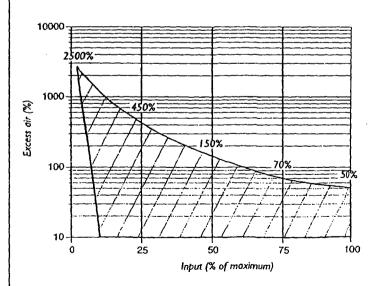


The emissions from the burner are influenced by:

- the fuel type
- the combustion air temperature
- · the firing rate
- the chamber conditions
- the percent of excess air.

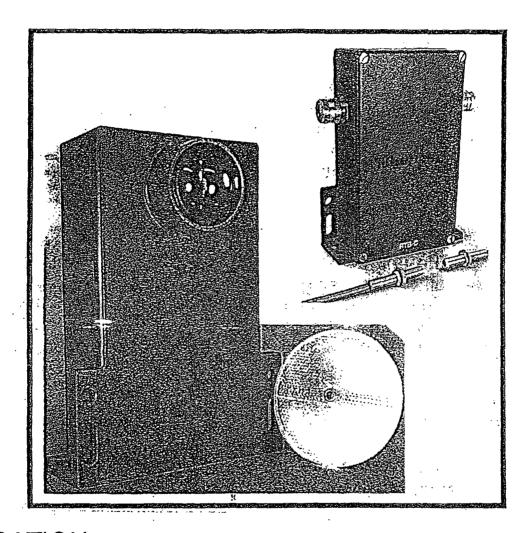
For estimates of other emissions, contact Eclipse Combustion.

Figure 3.3 Operational zone





## VISIBLE EMISSIONS ALARM (VEA)



APPLICATION: Alarm and control for <u>Opacity</u> used on small and large sources for warning operators and shutting down systems based on opacity, haze or clarity.

- Proven Rugged Design
- Unaffected by Ambient Light
- Spans up to 6 Feet
- Visible LED Light Source

- Dual Beam or Single Beam
- Adjustable Delay up to 3 min.
- Easy to Install & Support
- External Adjustment

## GENERAL PURPOSE OPACITY ALARMS



APPLICATION:

These units are specifically designed to

provide an operator with a reliable alarm system when Opacity or Smoke has exceeded a predefined limit. The alarm limit is easily set by using an opacity filter. The pulsed visible LED is <u>unaffected</u> by ambient light which makes for easy to install and calibrate.

**FEATURES:** 

The unit comes in either a single beam and dual

beam design and an almost permanent LED light source. The electronics are housed in a rugged die-cast housing and powered by either 120 VAC or 230 VAC.

These designs meet all common installation requirements.

#### SPECIFICATIONS:

LIGHT SOURCE: Pulsed Visible LED.

SPECTRAL RESPONSE: Between 400nm & 500nm.
ANGLE OF VIEW: Less the 4 degrees from axis

AMBIENT LIGHT: No measurable effect

RANGE: 0 TO 100% Opacity.

ACCURACY: +/- 3% of full scale.

ALARMS: DPDT 5.0 A @ 120 VAC; 100% adj.

LED indicator for alarm setting.

OTHER OUTPUTS: ON-OFF operation (no time delay).

OFF time delay (reverse of normal).

Adjustable One-shot

POWER: 100-130 Volts AC, 50/60 Hz, 10 VA.

TEMPERATURE: Ambient -20 to +150 degrees F.

Storage: +20 to +90 degrees F.

ENCLOSURES: Meet NEMA 3,4,5,12.

PHYSICAL: ELECTRONICS 8.0' x 5.75' x 3.31' (HWD).

VEA-S SINGLE BEAM - 3/8\*-24 inch. Straight Thread.

VEA-D DUAL BEAM SENSOR - 3" Diameter.

RESPONSE TIME: Selectable & Adjustable up to 3 minutes.

OPTOMONITOR, Inc. 270 Polaris Avenue Mountain View, CA 94043 Phone: 415/967-8992

Fax: 415/967-0286

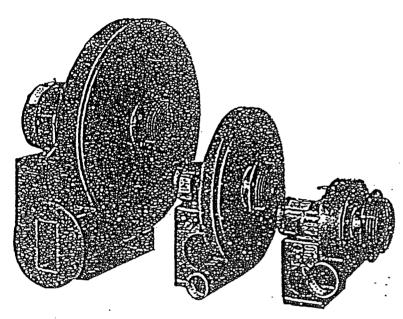
PLACE

STAMP

HERE

#### **ECLIPSE TURBO BLOWERS**

SERIES "SMJ"



- High efficiency
- Heavy gauge steel base and housing
- Aluminum impellers balanced statically and dynamically
- Matching air filters available
- Changeable outlet positions

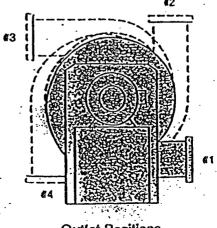
Eclipse "SMJ" Blowers are centrifugal blowers that provide low pressure air for industrial combustion systems. They are also used for cooling, conveying, drying, liquid agitation, smoke abatement, vacuum deaning, fume and dust exhausting, and other plications where air temperatures are under 220°F.

All "SMJ" Blowers are constructed of continuous welded, heavy gauge steel. The impellers are made of lightweight, high strength, riveted aluminum. Outlets on 3" and 4" models are threaded, while all others are flanged for a standard 125# ANSI companion flange. Discharge ports are sized to keep pressure losses within reasonable limits.

Blower inlet flanges are equipped with a grill that complies with OSHA regulations. If desired, the grill may be removed and the inlet bolted to a standard ANSI companion flange. Eclipse-supplied motors are standard shaft and starting torque, ball bearing, 3600 rpm units. On any blower requiring 3/4 HP or more, Eclipse recommends that polyphase motors be used.

There are four possible outlet positions. Any existing position is easily changed by removing the housing from the blower base and remounting it in the desired position. Positions 1 through 3 can be specified for any blower. Position 4, however, requires factory approval before ordering. Position 1 is the standard assembly (bottom, horizontal) unless otherwise specified.

"SMJ". Blowers can be supplied with counterclockwise (CCW) or clockwise (CW) rotation as viewed from the motor side. CCW rotation is furnished standard unless otherwise specified.

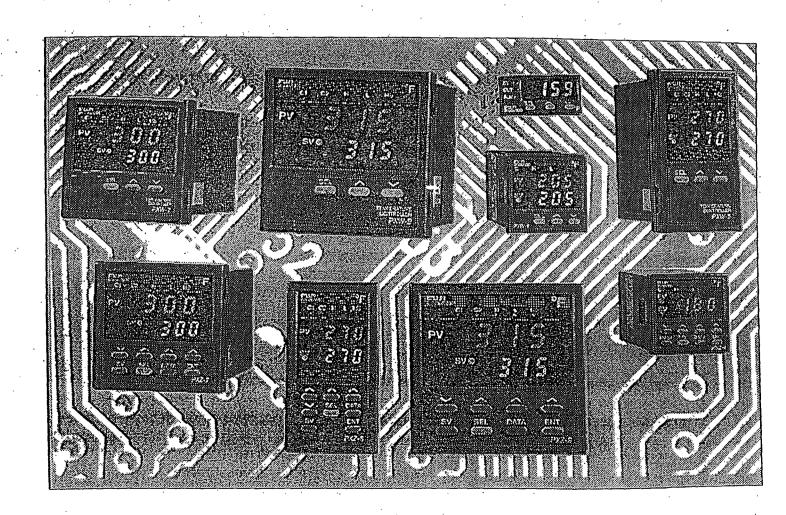


**Outlet Positions** 



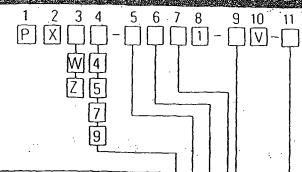


PID Autotune Controllers Featuring Fuzzy Logic



**Operation Manual** 

## MODELCONEGURATION



Front panel size	Code
48 x 48 (1/16DIN)	4
48 X 96 (1/8 DIN)	5
72 x 72 (72mm)	. 7
96 x 96 (1/4 DIN)	9

Kinds of input	Code
Thermocouple (°C)	T
Thermocouple (°F)	R
RTD/Pt100 (°C)	N
RTD/Pt100 (°F)	s
4-20mA DC, 1-5V DC	В
0-20mA DC, 0-5V DC	. A

Control output 1	Code
Relay contact (reverse action)	Α
Relay contact (direct action)	8
SSR driver (reverse action)	C
SSR driver (direct action)	0
4 to 20mA DC (reverse action)	€.
4 to 20mA DC (direct action)	F

Control output 2*	Code
None	Y
Relay contact (reverse action)	A
Relay contact (direct action)	В
SSR driver (reverse action)	C
SSR driver (direct action)	0
4 to 20mA DC (reverse action)	3
4 to 20mA DC (direct action)	F

\*not available on 48 x 48mm type

Additional function	Code
Heater break alarm*	2
Process alarm &	
Heater break alarm"	3
None	4
Process alarm	5

\*not available on 48 x 48mm type

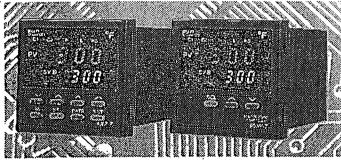
Power Supply Option	Code
24V AC/DC Supply	D:

## FAURES

- 1/4 DIN, 1/8 DIN, 72mm, 1/16 DIN and 1/32 DIN sizes available
- Choose between 3-button or 8-button operation
- Fuzzy logic control with PID Autotune
- Universal input-T/C, RTD, current, and voltage
- 24V DC/AC supply option available
- 8 segment ramp/soak programming
- Advanced security options to prevent unauthorized changes in parameters
- NEMA 4X faceplate

#### GENERAL SPECIFICATIONS

Rated voltage	85-264V AC or 24 AC/DC
Power consumption	10VA or less (100V AC, without option) 15VA or less (220V AC, without option)
Insulation resistance	50M $\hat{\Omega}$ or more (500V DC)
Withstand voltage	Power source-Earth: 1500V AC, 1 min Power source-Other: 1500V AC, 1 min Earth-relay output: 1500V AC, 1 min Earth-Alarm output: 1500V AC, 1 min Other: 500V AC, 1 min
Input impedance	Thermocouple: 1M $\Omega$ or more Voltage: 450K $\Omega$ or more Current: 250 $\Omega$ (external resistor)
Allowable signal source resistance	Thermocouple: 100 (O or more Voltage: 1K (O or more
Allowable wiring resistance .	RTD: 10 Ω or less per wire
Reference junction compensation accuracy	± 1.°C (at 23°C)
Process variable offset	(PV shift)±10% FS
Set variable offset	± 50% FS
Input filter	0-120.0 sec. setting in 0.1 sec steps (primary lagging filter)
Noise reduction ratio	Normal mode noise (50/60Hz): 50dB or more Common mode noise (50/60Hz): 140dB or more



#### PXZ and PXW 7

#### **POWER FAILURE PROCESSING**

Memory protection:	Non-volatile memory hold
• •	Non-volatile memory hold  After the recovery of power, control is started
·	 at the value before power failure:

#### SELF-CHECK

Method:	Watchdog timer monitors program error.

#### **OPERATION AND STORAGE CONDITIONS**

Operating temperature	-10 to 50°C
Operating humidity	90% RH or less (non-condensing)
Storage temperature	-20 to 60°C

#### CONTROL FUNCTION

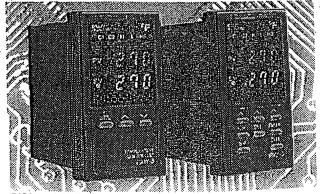
	-	_		-		•	-	_	-	-	_	-	-	_	-	
1	S	T.	۸	1	J	r	)	٨	BI	)	1	Y	ç	ŗ	)	

Control action	PID control with auto-tuning Fuzzy control with auto-tuning
Proportional band (P)	0-999.9%, setting in 0.1% steps
Integral time (I)	0-3200 sec, setting in 1 sec steps
Differential time (D)	0-999.9 sec, setting in 1 sec steps
P.I.D= 2-Pt. Position action Proportional action when	
Proportional cycle	1-150 sec. setting in 1 sec steps, relay contact output, SSR/SSC drive output only
Hysteresis width	0-50%, setting in 1% steps, 2-position action only
Anti-reset wind up	0-100% FS, setting in 1% steps; auto-setting with auto-tuning
Input sampling cycle	0.5 sec
Control cycle	0:5 sec

#### CONTROL FUNCTION

(DUAL OUTPUT TYPE) (HEATING/COOLING TYPE)

Heating Proportional band	P x 1/2 (P= 0.999.9%)
Cooling Proportional band	Heating proportional band x cooling proportional band coefficient Cooling proportional band coefficient=0-99.9 0:2- position action
lutegral time	0:3200 sec for heating and cooling
Differential time	0-999.9 sec for heating and cooling
P.I.D= 0:2- position action (I.D= 0:Proportional action	without dead band) for heating and cooling
Proportional cycle	1-150 sec; relay contact output, SSR/SSC drive output only
Hysteresis width	2-position action for heating and cooling: 0.5% FS 2-position action for cooling: 0.5% FS
Anti-reset wind-up	0-100% FS; setting in 1% steps, auto setting with auto-tuning
Overlap/dead band :	±50% of heating proportional band
Input sampling cycle .	0.5 sec
Control cycle	0.5 sec



PXW and PXZ 5

# EMISSIONS TESTING of the FOSTER'S PET CREMATION SERVICE B & L SYSTEMS, INC. BLP 500/150 ANIMAL CREMATORY INCINERATOR Spring Hill, Florida

March 9, 2004

FDEP Permit No.: 1010377-002-AO EU No. 003 SES Reference No. 04S61

#### Conducted by:

SOUTHERN ENVIRONMENTAL SCIENCES, INC. 1204 North Wheeler Street Plant City, Florida 33563 Phone (813) 752-5014, Fax (813) 752-2475

#### **Project Participants**

Mark S. Gierke Dale A. Wingler Travis B. Nelson

# EMISSIONS TESTING of the FOSTER'S PET CREMATION SERVICE B & L SYSTEMS, INC. BLP 500/150 ANIMAL CREMATORY INCINERATOR Spring Hill, Florida

March 9, 2004

#### **TABLE OF CONTENTS**

		<u>Page</u>
1.0	INTRODUCTION	1
2.0	SUMMARY OF RESULTS	1
3.0	PROCESS DESCRIPTION	4
4.0	SAMPLING PROCEDURES	4
	4.1 Methods 4.2 Sampling Locations 4.3 Sampling Trains 4.4 Sample Collection 4.5 Sample Recovery	4 5 5 8 <b>1</b> 0
5.0	ANALYTICAL PROCEDURE	11
	5.1 Pretest Preparation	11 11
API	PENDIX	. 12
	Project Participants Certification Visible Emissions Evaluation Process Operational Data Laboratory Data Temperature Recording Chart Field Data Sheets CO Analyzer Strip Chart Calculations and Symbols	

#### 1.0 INTRODUCTION

Southern Environmental Sciences, Inc. conducted emissions testing of the Foster's Pet Cremation Service animal crematory on March 9, 2004. This facility is located at 15204 County Line Road, Spring Hill, Florida. Testing was conducted for particulates, carbon monoxide and visible emissions. Oxygen (O<sub>2</sub>) concentrations were measured to correct emission rates to 7% O<sub>2</sub>. Testing was performed to determine if the plant was operating in compliance with requirements of the Florida Department of Environmental Protection (FDEP).

#### 2.0 SUMMARY OF RESULTS

The facility was found to be in compliance with all applicable emission limiting standards. Results of the particulate and carbon monoxide testing are summarized in Table 1. Particulate emissions from this source are limited to a maximum allowable concentration of 0.080 grains per dry standard cubic foot (corrected to  $7\% O_2$ ), and 0.30 pounds per hour. The average measured particulate concentration was 0.009 grains per dry standard cubic foot (corrected to  $7\% O_2$ ), and 0.031 pounds per hour, well within the limit. The maximum allowable carbon monoxide emissions concentration from this source is 100 parts per million, dry basis (corrected to  $7\% O_2$ ), and 0.17 pounds per hour. The average measured carbon monoxide emission concentration was 4.3 parts per million, dry basis (corrected to  $7\% O_2$ ), and 0.01 pounds per hour, well within the allowable limit.

A visible emissions evaluation was performed over a one hour period. The average

#### TABLE 1. EMISSIONS TEST SUMMARY

Company: FOSTER'S PET CREMATION SERVICE

Source: Animal Crematory Incinerator

	Run 1	Run 2	Run 3
Date of Run	3/9/04	3/9/04	3/9/04
Process Rate (lbs/hr)	124	124	124
Start Time (24-hr. clock)	1135	1302	1425
End Time (24-hr. clock)	1238	1403	1526
Vol. Dry Gas Sampled Meter Cond. (DCF)	35.293	36.3 <b>0</b> 8	37.298
Gas Meter Calibration Factor	0.986	0.986	0.986
Barometric Pressure at Barom. (in. Hg.)	30.14	30.14	30.14
Elev. Diff. Manom. to Barom. (ft.)	0	0	0
Vol. Gas Sampled Std. Cond. (DSCF)	34.324	34.476	35.476
Vol.: Liquid Collected Std. Cond. (SCF)	8.020	6.794	5.913
Moisture in Stack Gas (% Vol.)	18.9	16.5	14.3
Molecular Weight Dry Stack Gas	29.04	29.12	29.30
Molecular Weight Wet Stack Gas	26.95	27.29	27.69
Stack Gas Static Press. (in. H2O gauge)	-0.01	-0.01	-0.01
Stack Gas Static Press. (in. Hg. abs.)	30.14	30.14	30.14
Average Square Root Velocity Head	0.164	0.175	0.178
Average Orifice Differential (in. H2O)	1.049	1.041	1.118
Average Gas Meter Temperature (°F)	80.6	93.7	92.9
Average Stack Gas Temperature (°F)	1240.3	1367.1	1359.6
Pitot Tube Coefficient	0.84	0.84	0.84
Stack Gas Vel. Stack Cond. (ft./sec.)	17.01	18.68	18.85
Effective Stack Area (sq. ft.)	1.77	1.77	1.77
Stack Gas Flow Rate Std. Cond. (DSCFM)	457	482	501
Stack Gas Flow Rate Stack Cond. (ACFM)	1,803	1,981	1,999
Net Time of Run (min.)	60	60	60
Nozzle Diameter (in.)	0.611	0.611	0.611
Percent Isokinetic	108.7	103.6	102.5

TABLE 1. EMISSIONS TEST SUMMARY (con't)

Company: FOSTER'S PET CREMATION SERVICE

Source: Animal Crematory Incinerator

· · · · · · · · · · · · · · · · · · ·	•	•		
	Run 1	Run 2	Run 3	
Date of Run	3/9/04	3/9/04	3/9/04	
Process Rate (lbs/hr)	124	124	124	
Start Time (24-hr. clock)	1135	1302	1425	
End Time (24-hr. clock)	1238	1403	1526	
Oxygen (%)	8.0	10.0	10.5	
				Average
Particulate Collected (mg.)	34.0	11.1	7.4	
Particulate Emissions (gr./DSCF)	0.015	0.005	0.003	0.008
Particulate Emissions (gr./DSCF @ 7% 02)	0.016	0.006	0.004	0.009
Allowable Part. Emissions (gr./DSCF @ 7% O2)				0.080
Particulate Emissions (lb./hr.)	0.060	0.021	0.014	0.031
Allowable Part. Emissions (lb./hr.)				0.30
CO Emissions (PPM)	3.08	2.25	5.00	4.3
CO Emissions (PPM @ 7% O2)	3.3	2.9	6.7	4.3
Allowable CO Emissions (PPM @ 7% O2)				100
CO Emissions (lb./hr.)	0.006	0.005	0.011	0.007
Allowable CO Emissions (lb./hr.)			, •	0.12
· · · · · · · · · · · · · · · · ·				

Note: Standard conditions 68°F, 29.92 in. Hg

maximum six minute opacity was zero percent, well within the allowable limit of 5 percent.

#### 3.0 PROCESS DESCRIPTION

The B & L Systems, Inc. Model BLP 500/150 Series crematory incinerator cremates animal remains in an environmentally acceptable manner. Emissions are controlled by an afterburner. The afterburner is preheated and maintained at a minimum operating temperature of 1600°F prior to ignition of the primary chamber. The unit is designed to be charged with a maximum of 500 pounds of animal remains and incinerate at a maximum rate of 150 pounds per hour with a maximum heat input of 1.35 MMBTU per hour (primary chamber 0.35 MMBTU per hour, secondary chamber 1.0 MMBTU/hr), each chamber fired exclusively on propane gas only. The time required for complete incineration depends upon the total weight of the waste. Process operational data was provided by facility personnel and is included in the appendix.

#### 4.0 SAMPLING PROCEDURES

#### 4.1 Methods

All sampling was performed using methods currently acceptable to the FDEP. Particulate sampling and analyses were conducted in accordance with EPA Method 5 - Determination of Particulate Emissions from Stationary Sources, 40 CFR 60, Appendix A-3. Carbon monoxide emissions were conducted in accordance with EPA Method 10 - Determination of Carbon Monoxide Emissions from Stationary Sources, 40 CFR 60, Appendix A-4. The oxygen content of the stack gas was determined in accordance with EPA Method 3B - Gas

Analysis for the Determination of Emission Rate Correction Factor or Excess Air, 40 CFR 60, Appendix A-2. The visible emissions evaluation was performed using procedures described in EPA Method 9 - Visual Determination of the Opacity of Emissions from Stationary Sources, 40 CFR 60, Appendix A-4.

#### 4.2 Sampling Locations

Locations of the sample ports and stack dimensions are shown in Figure 1. Particulate sampling was accomplished by conducting horizontal traverses through each of two ports located on the stack at a ninety degree angle from one another. Twenty four sample points were chosen in accordance with EPA Method 1 - Sample and Velocity Traverses for Stationary Sources, 40 CFR 60, Appendix A-1. Carbon monoxide and oxygen sampling were performed from the same sampling ports as the particulate sampling.

#### 4.3 Sampling Trains

The particulate sampling train consisted of a Nutech Corporation 3 foot quartz lined probe and nozzle, a heated glass fiber filter and four impingers arranged as shown in Figure 2. Flexible tubing was used between the heated filter and the impingers. The first two impingers were each charged with 100 milliliters of water, the third served as a dry trap and the fourth impinger was charged with indicating silica gel desiccant. The impingers were cooled in an ice and water bath during sampling. A Nutech Corporation control console was used to monitor the gas flow rates and stack conditions during sampling.

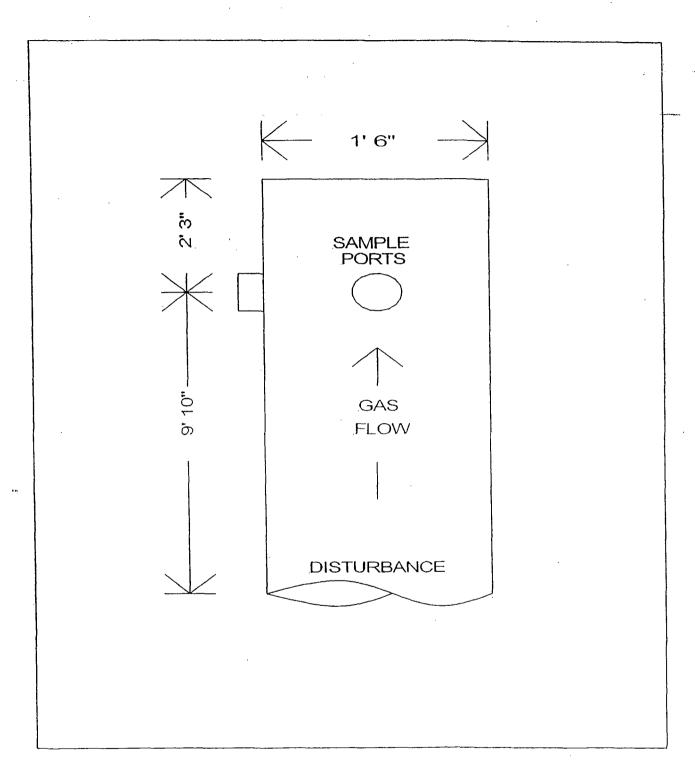


Figure 1. Stack Dimensions and Sample Port Locations, Foster's Pet Cremation Service, Animal Crematory Incinerator, Spring Hill, Florida.

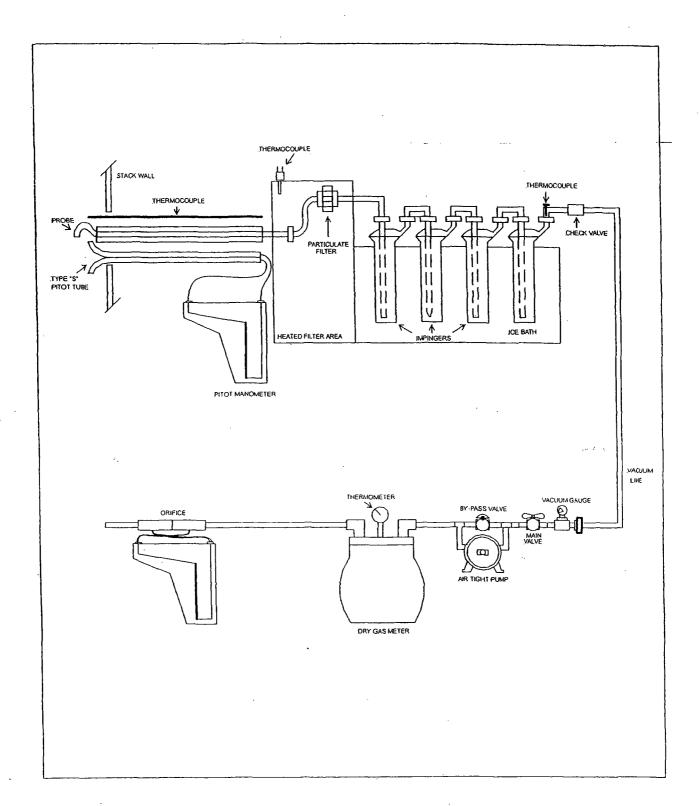


Figure 2. EPA Method 5 Sampling Train.

The carbon monoxide sampling train consisted of a stainless steel probe, teflon sample line, condenser, silica gel and carbon dioxide adsorbent tubes and a Thermo Environmental Instruments, Inc. Model 48 Gas Filter Correlation CO analyzer arranged as shown in Figure 3. The oxygen sampling train consisted of a probe, sample line, tedlar bag in a rigid container, valve, vacuum pump, and flow meter.

#### 4.4 Sample Collection

Prior to particulate sampling, the pitot tubes were checked for leaks and the manometers were zeroed. A pretest leak check of the particulate sampling train was conducted by sealing the nozzle and applying a 15" Hg vacuum. A leak rate of less than 0.02 cubic feet per minute was considered acceptable. Particulate sample was collected isokinetically for two and one half minutes at each of the points sampled.

The carbon monoxide analyzer was calibrated immediately prior to the beginning of the test and checked after each run by introducing known gases into the instrument through the sampling train.

The tedlar bag used for obtaining an integrated oxygen sample was leak checked prior to the test by pressurizing it to 2 to 4 in. H<sub>2</sub>O and allowing it to stand overnight. The bag was considered leak free if it remained inflated. A one hour integrated sample was obtained at a rate 0.5 liters per minute for each run.

Carbon monoxide and oxygen sampling were conducted simultaneously with particulate

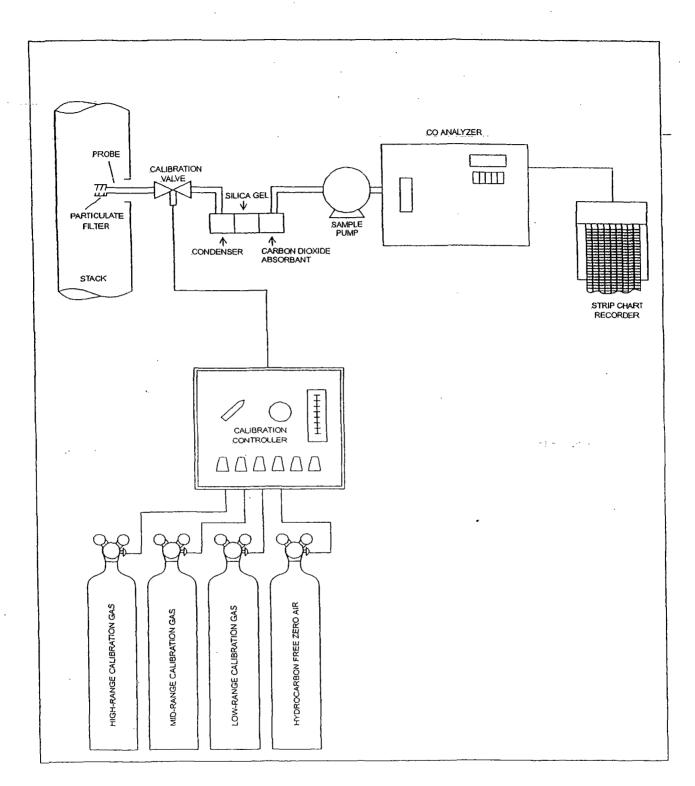


Figure 3. EPA Method 10 Sampling Train.

sampling.

#### 4.5 Sample Recovery

A post test leak check of the particulate sampling train was performed at the completion of each run by sealing the nozzle and applying a vacuum equal to or greater than the maximum value reached during the sample period. A leak rate of less than 0.02 CFM or 4 percent of the average sampling rate (whichever was less) was considered acceptable. The nozzle and probe were then brushed and rinsed with reagent grade acetone and the washings were placed in clean polyethylene containers and sealed. The glass fiber filter was removed from the holder with forceps and placed in a covered petri dish for return to the laboratory. The front half of the filter holder was rinsed with acetone and the washings were added to the nozzle and probe wash. The contents of the first three impingers were measured volumetrically and the silica gel in the fourth impinger was weighed to the nearest 0.1 gram for determination of moisture content.

Two calculations of the moisture content of the stack gas were made for each run, one from the impinger analysis and one from the assumption of saturated conditions based upon the average stack gas temperature and a psychrometric chart as described in EPA Method 4, Determination of Moisture Content in Stack Gases, 40 CFR 60, Appendix A. The lower of the two values of moisture content was considered to be correct and was used in the emissions computations.

#### 5.0 ANALYTICAL PROCEDURE

#### 5.1 Pretest Preparation

The glass fiber filters for the particulate train were numbered, oven dried at 105°C for two-to three hours, desiccated and weighed to a constant weight in preparation for the test. Results were recorded to the nearest 0.1 milligram. Filters were loaded into holders and a filter was set aside as a control blank. The impingers were charged as described in section 4.3 and the contents of the fourth impinger were weighed to the nearest 0.1 gram.

#### 5.2 Analysis

Upon return to the laboratory, the particulate filters were removed from the containers with forceps, dried at 105°C for two to three hours, desiccated and weighed to a constant weight. Results were recorded to the nearest 0.1 milligram. The probe and nozzle washes and an acetone blank were measured volumetrically and transferred to clean, tared evaporating dishes and evaporated to dryness over low heat. The evaporating dishes were then oven dried at 105°C for two to three hours, desiccated and weighed to a constant weight. Results were recorded to the nearest 0.1 milligram. The total particulate reported is the sum of the filter weight gain and the weight gain of the evaporating dishes, corrected for the acetone blank.

#### **APPENDIX**

**Project Participants** 

Certification

Visible Emissions Evaluation

Process Operational Data

Laboratory Data

Temperature Recording Chart

Field Data Sheets

CO Analyzer Strip Chart

Calibration Data

Calculations and Symbols

#### PROJECT PARTICIPANTS AND CERTIFICATION

# FOSTER'S PET CREMATION SERVICE B & L SYSTEMS, INC. BLP 500/150 ANIMAL CREMATORY INCINERATOR Spring Hill, Florida

March 9, 2004

#### Project Participants:

Mark S. Gierke Dale A. Wingler Travis B. Nelson Conducted the field testing.

Fred T. Smith II (Foster's Pet Cremation)

Provided process rates.

Mark S. Gierke

Performed visible emissions

evaluation.

Kenneth M. Roberts

Performed laboratory analyses.

Dale A. Wingler

Prepared the final test report.

#### Certification:

I certify that to my knowledge all data submitted in this report is true and correct.

Mark S. Gierke

## SOUTHERN ENVIRONMENTAL SCIENCES, INC. 1204 North Wheeler Street, Plant City, Florida 33566 (813)752-5014

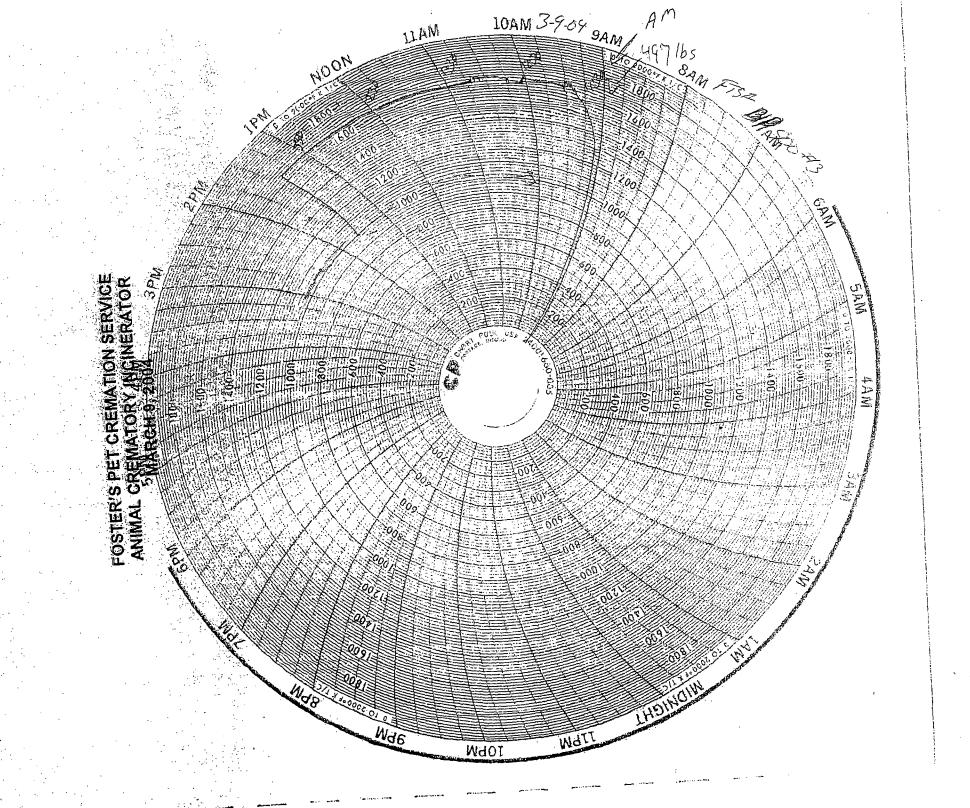
### VISIBLE EMISSIONS EVALUATION

COMPANY FUSTLY'S P	et Cramation Service						
UNIT Anima Crama	and the second of the second o						
ADDRESS 15204 COUNTY RING Rd							
Spring Hill, FL							
PERMIT NO. 1010377-002-40	COMPLIANCE? YES TO D						
AIRS NO. 1010377 EUNO. 003							
PROCESS RATE 497 (6 BYTCH)	PERMITTED RATE 500 (3 Datch						
PROCESS EQUIPMENT BYL SUO/150 Crama TUYY							
CONTROL EQUIPMENT AFTA	1 bulner						
OPERATING MODE Nat. Gas Fived	AMBIENT TEMP. (°F) START 70 STOP 75						
HEIGHT ABOVE GROUND LEVEL START STOP SIME	HEIGHT REL. TO OBSERVER STARTN JO'STOP						
DISTANCE FROM OBSERVER STARTNEO STOP SOME	DIRECTION FROM OBSERVER START 3500 STOP 3500						
EMISSION COLOR NONE	PLUME TYPE N/A CONTIN. D INTERMITTENT D						
WATER DROPLETS PRESENT NO YES []	IS WATER DROPLET PLUMEN / ATTACHED & DETACHED &						
POINT IN THE PLUME AT WHICH STARTS TOLCK Exit							
DESCRIBE BACKGROUND START SKY	STOP same						
BACKGROUND COLOR STARTCYBILW MISTOPSOME	SKY CONDITIONS START SEGIT STOP STYLL						
WIND SPEED IMPHI START 3-10 STOP SUM	WIND DIRECTION START 5 STOPS						
AVERAGE OPACITY FOR OF HIGHEST PERIOD	RANGE OF OPAC, READINGS MIN. MAX.						
SOURCE LAYOUT SKETCH	O DRAW NORTH ARROW						
0	Emission Point						
Sun * Wind Plume and Stack	Observer's Position						
Sun Location Line							
COMMENTS SOTIOL # 20	03-17-93						
#3 Incinerator							

OBSERV	ATION	DATE	ST	ART TIN	ЛE	T	STOP TI	ME_		
SEC	0 1	15	30	45	SEC	0	15	30	45	
MIN				, ,	MIN		1 2	0.0		
0	0	0	0	0	30	0	5		5	
1	0	0	0	0	31	0	0	0	0	
2	0	Ó	0	0	32	0	0	0	0	
3	0	0	0	0	33	0	0	0	0	
4	0	0	0	0	34	0	0	0	0	
5	0	0	0	0	35	0	0	0	0	
6	0	0	0	0	36	0	0	0	0	
7	10	0	0	0	37	0	0	0	0	
8	0	0	10	0	38	0	0	0	0	1
9	0	0	10	10	39	10	10	0	0	,¶
10	10	C	10	10	40	10	0	0	10	4
11	10	10	10	10	41	10	10	0	10	-
12	10	10	10	19	42	10	10	10	$\Box$	-
13	16	100	10	10	43	15	10	10	10	4
14	(5)			10	44	15	19	18	10	겝.
15	10	1			45	10		12	1	1
16	16	14	10	10	46	10		10		-
17	10	15	12		47	16		10	15	$\mathbb{H}$
18	10	) F			48	10	10	5		ᆐ
20	1 4		10		50	19	116	10	15	$\exists$
21	10				51	10	10	15		1
22	10		5		52	1	7/2	1	1/	3
23	1	9 6			53	1	5/6	5 6	<u>5</u>	케
24	7		1/	10	54	7	10	8		7
25			2 0		55	16		1	) 7	$\frac{1}{2}$
26			5/2	, –	56	1		) (	3/	51
27	7	7			57	1		7	7	7
28	(				58		dô		5 2	51
29	(**	517		- 7	59		00	1 6		
Ob	Observer: Mark Girkha									
Ce	Certified by: FNx D Certified at: Tig MPG									
Da	Date Certified: 204 Exp. Date: 8/01									
	I certify that all data provided to the person conducting the test was true and correct to the best of my knowledge:									
Sig	natur	e: (	Jee	Pro	025	<u>5 \</u>	,)+·	514	T, M,	, [
Ti+										

### PROCESS WEIGHT STATEMENT

DATE 3/9/04 SAME	PLING TIME: FROM 11:35 A.M. TO 3:25 P.M.
STATEMENT OF PROCESS WEIGHT	
COMPANY FOSTEL'S P	et Cremation Service
	ounty Line Rd.
	FL 34610
· · · · · · · · · · · · · · · · · · ·	ematory Incinerator
SOURCE LOCATION Spring H.	11, FL
DATA ON OPERATING CYCLE TIME	
END OF OPERATION, TIME	· · · · · · · · · · · · · · · · · · ·
ELAPSED TIME	
IDLE TIME DURING CYCLE	
DESIGN PROCESS RATING PROCESS WEI	GHT RATE (INPUT)
원	RODUCT (OUTPUT)
,	* 497 165/Batch
DATA ON ACTUAL PROCESS RATE DU	
MATERIAL AnimaL Bodies	RATE R#1 124 165/60
MATERIAL 1, 1,	100111
AVERAGE PROCESS V	<u> </u>
PRODUCT	RATE
PRODUCT	HATE
PRODUCT	RATE
I certify that the above information is true	and correct to the best of my knowledge.
Name (Pl	LEASE PRINT) TREAT Jun HI
,	Signature Jan 1 State
	Title Oferator



#### PARTICULATE MATTER COLLECTED

Plant: Unit No. FOSTER'S PET CREMATION SERVICE ANIMAL CREMATORY INCINERATOR

Weight of particulate matter, g.

0.0074

Test Date: 03/09/2004		Analyzed by:	DW		<del></del>
Acetone blank container no. Acetone blank volume, ml.,(Va) Acetone blank final weight, g. Acetone blank tare weight, g. Acetone blank weight diff.,g.,(ma)	10 20 104.216 104.215 0.000	0 Filter bla 3 Filter bla 9 Filter we	ank no. ank tare wei ank final we eight diff., g	ight, g.	7158 0.3691 0.3692 0.0001
Run No. Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml. (Vaw) Acetone wash residue, g. (Wa)	1 7111 0 23 100 0.0002	Number Ethal  1 (Filter) 2 (Wash)  Less	0.3935 00.6231	REIGULATE 6 0.367 100.6154 TOTAL ank, g. (Wa)	0.0265 0.0077 0.0342 0.0002
Run No. Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml. (Vaw) Acetone wash residue, g. (Wa)	2 7113 0 43 95 0.0002	Container WE Number Final  1 (Filter) 2 (Wash)	0.3686 108.7303	ARTICULATE Tare Weight  0.3661 108.7215  TOTAL  lank, g. (Wa) late matter, g.	0.0340 20LLECTED 0.002 0.008 0.011
Run No. Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml. (Vaw Acetone wash residue, g. (Wa)	3 7117 0 4 105 0.0002	Nimber Lina  1 (Filter) 2 (Wash)	0.3695 103.1044	ABTICULATE  ABTICULATE  0.3692 103.0971  TOTAL  plank, g. (Wa)	

### MOISTURE COLLECTED

Plant	Foster's Chemotory					·
Unit Date Run N	Animal Incinctator 3/4/04					
	Impinger Number	1	2	3	4	Weighed by:
	Final Weight (grams):	0.006	100.0	0	261.0	CSE
	Initial Weight (grams):	100 0	100.0	<u></u>	250.9	(D)
	Difference (grams):	160.0	<u> </u>	0	10.1	
	Total Condensate (grams):				170.1	
Unit Date Run N	Amna Incinetator 3/9/04 No. 201 2	·	·			
	Impinger Number	1	2	3	4	Weighed by:
	Final Weight (grams):	230.0	106.0	0	253.9	(IX)
	Initial Weight (grams):	100.0	100.0	0	245.8	
·	Difference (grams):	130,0	6.0	0	8.1	
	Total Condensate (grams):				144.1	
Unit Date Run I	Amm Inchestile 3/9/04 No3					
	Impinger Number	1	2	3	4	Weighed by:
	Final Weight (grams):	210.0	106.0	<u>. C</u>	255.0	
	Initial Weight (grams):	100.0	1000		245.6	The state of the s
	Difference (grams):	110.0	6.0	0	9.4	
•					1	•

Page \_\_\_\_ of \_\_\_

#### FIELD DATA SHEET

4-1:	/\ i						
Company tosles	( tematery			Run Numt	er		
Source Animal	Ciematory.	Incinerator.	<u> </u>	Da	ate	3/9/04	
Operator(s)	wher / !	- Welson		24 hr Time at St	art	1135	
	0 7		•	24 hr Time at E	nd	1238	
Dimensions Diak				Filter No	s).	7111	
LxW□	K"			Barometric Pressure ("1	-dg)	3014	
Static Press. ("H2O)	- 20 i		Elev	Diff. Mano. To Barom.	Ft)	0	
Meter Box No.	002			Ambient Temperature	(°F)	68	
Meter ∆H@	1.726	Assumptions					
Meter Correction Factor	,98G	% Moisture	14	Sample Train Leak Che	ck:		
Pitot Tube Cp	.84	Stack Temp.	1000/1200	Initial 0.002 C	FM @		"Hg
Nozzle ID	Quartz	Meter Temp.	75	Final 0.00 2 C	FM @_	10	"Hġ
Nozzle Dia. (Inches)	-611	Md/Ms	1,05	Initial Pitot Tube (-)	/+	1	
Probe Length/Liner	3' Questz	K Factor			(+	1	
	- • •			* 0-,25" Mugnehl	16 USe1	) ¥	
Moist, Collected: Imp. No.	1 , Imp. N	o. 2 & 3 , Im	p. No. 4'	, Total Filter	Tare Wt,	, .	

Point								ilter Tare		
No.	Sample Time (min.)	Meter Vol. Vm (ft³)	Vel. Head ΔP ("H <sub>2</sub> O)	Orifice Diff. ΔΗ ("H <sub>2</sub> O)	Stack Temp.,Ts (°F)	Meter Temp., Tm (°F)	Hot Box Temp. (°F)	Exit Temp. (°F)	Pump Vacuum ("Hg)	Other
1	0	045.727	.02	185	1350	66	269	63	J. O	
2	2.5	47.10	,04	1.7	1349	67	269	63	J.O	
3	.5	48.67	,(4	6.7	1358	18	267	62	3.0	
4	7.5	50,66	:02	,85	1323	70	265	62	1.5	
5	10	52.04	,02	,45.	1299	71	265	Ci	1.5	
6	12.5	53.36	, 02	.55	1280	7.2	269	62	1.5	ļ
7	15	54.68	225	29:3	1194	73	265	61	2.0.	ļ
8	17.5	56.t3	,035	,93	1170	74	264	GI	1.5	<u> </u>
9	20	57.43	.02	85	1113	76	25%	60	i.5	
10	42.5	63.77	,025	.93	1119	77	249	60	20	
11	25	60.10	.625	.93	1152	78	257	66	2.0	<u> </u>
12	275	61.54	:025	.93	1180	80	257	159	2.0	
13	30	C2.92	.63	1.1)	1134	81	256	59	3,6	
14	37.5	C4.42	,03	11)	1142	83	255	59	3.0	
15 }	35	65.95	εο,	1.12	1197	84	252	59	3.5	
16	37.5	67.16	.035	1.31	1135	85	260	58	4.0	
17	40	69.15	,035	1.31	1241	87	267	58	4.0	
18 ¢	42.5	70.33	.03	1.12	1254	89	268	159	40	
19	45	72.40	025	.93	1275	90	262	58	3.5	
20	47.5	73.53	.075	.93	1289	91	268	58	3.5	
21 9	50	75,22	_025	.93	1274	92	263	53	3.5	1
22	55.5	76.65	,035	-93	1250	9:3	258	58	3,5	
23	55	78.06	,03	1./2	1281	94	252	57	40	+
24	57.5	79.58	,025		1281	94	247	58	4.0	
<b></b>	60	81.020	+ * ~ ~ ~ ~	<del>                                     </del>	1	<del></del>	1	1 -	1 - 1	

FIELD DATA SHEET

Page \_\_ of \_\_

Company Fostris Source Anima Operator(s) Dimensions Dia	Pet Crements I Cirminates ingles / T	Nelson		Run Number Date 24 hr Time at Start 24 hr Time at End Filter No(s). Barometric Pressure ("Hg)	3/9/04 1362 1403 7//3 30,14	
Static Press. ("H2O)			Elev	Diff. Mano. To Barom. (Ft)	0	
Meter Box No. Meter ΔH@	1.726	Assumptions	·	Ambient Temperature (°F)		
Meter Correction Factor	. 98C	% Moisture	120018	Sample Train Leak Check:		
Pitot Tube Cp	84	Stack Temp.	1350	Initial 6.000 CFM	@ /5	"Hg
Nozzle ID	Quartz	Meter Temp.	9	Final o.co.2 CFM	@ 10	"Hg
Nozzle Dia. (Inches)	-G11	Md/Ms	ind	Initial Pitot Tube (-)	(+1	
Probe Length/Liner	3' quartz	K Factor	33.18	Final Pitot Tube (-)	(+)	

oist. Co	llected:- lm	ρ. No. 1	Imp. No. 2 &	. კ , In	np. No. 4		+ <del></del>	ilter Tare	Wt,	
Point No.	Sample Time (min.)	Meter Vol. Vm (ft³)	Vel. Head ΔP ("H₂O)	Orifice Diff. ΔΗ ("H₂O)	Stack Temp.,Ts (°F),	Meter Temp., Tm (°F)	Hot Box Temp. (°F)	Exit Temp. (°F)	Pump Vacuum ("Hg)	Othe
1	0	43.822	,03	102	1190	39	-241	64	1.0	
2	2.5	85.35	3	7.77	TELEPLE.	<b>9</b> 9	242	64	1.0	
3	5	86.86	1055	1.19	1356	90	240	64	1.0	<u> </u>
4	7.5	88.43	.09	636	1324	91	241	63	1.0	
5	jo	901)	, 6	1.30	1380	92	255	63	1.5	
6	125	91.84	04	1.36	1395	-23	263	63	1.5	<u> </u>
7	15	93,57	,03	(.0)	1338	93	269	63	1.0	
8	17.5	95.07	63	1.0)	1398	94	267	62	1.0	<u> </u>
9	20	96,57	.03	1.0.2	1390	94	1260	63	1.0	<u> </u>
10	22.5	98.07	.03	1.02	1380	94	263	62	1.0	
11	25	99.57	,03	1.02	1377	94	261	62	1.0	
12	27.5	101.07	.03	1.02	1387	94	257	62	1.0	
13	30	162.56	.03	1.02	1364	94	268	61	1.0	
14	325	104.09	,03	1.02	1377	94	270	161	1.0	
15 }	35	105,58	, 035	1.19	1376	94	268	60	1.0	]
16	37.5	107.18	103	1.02	1382	194	203	60	10	
17	40	108.68	,03	1.02	/399	95	267	60	1.0	
18 (,	42.5	110.2	:035	1.19	1407	95	270	58	20	
19	45	111.79	.025	,85	1382	96	257	158	1.0	
20	47.5	113.75	:025	.85	1369	96	1248	58	10	1
21 9		114.C2	1025	195	1368	96	1246	58	1.0	1
22	55.5	116.00	.025	85	1369	96	243	58	1.0	<del>                                     </del>
23	55	117.37	025	,85	1377	9G	1241	157	1.0	+-
24	525	118,75	1,025	,35	1368	96	244	57	1.0	+-
<del></del>	60	120.130	+	+-*	1089	+-'¥	1/2/	121	1-0	

FIELD DATA SHEET

Page \_\_\_ of \_\_

٠, ،	N i	·			1
Company toster's	Tet Cremat.	ion Sevice		Run Number	3
Source Anima	1 Cirmatein			Date	3/9/04
Operator(s)	-1/ T	A Jelson	·	24 hr Time at Start	1425
(				24 hr Time at End	1576
Dimensions Diaky				Filter No(s).	27/17
LxW□	<u> 18" </u>			Barometric Pressure ("Hg)	30.14
Static Press. ("H20)	-,01			Elev Diff. Mano. To Barom. (Ft)	
Meter Box No.	000			Ambient Temperature (°F)	7)
Meter ∆H@	1.726	Assumptions		·	
Meter Correction Factor	786	% Moisture	<u> 12 </u>	Sample Train Leak Check:	
Pitot Tube Cp	- 184	Stack Temp.	1375	Initial 6.00,2 CFM	@ <u>/5</u> "Hg
Nozzle ID	Piritz	Meter Temp.	95	Final 0.602 CFIVI	@ <i>[()</i> "Hg
Nozzie Dia. (Inches)	<u></u>	Md/Ms	1.05	Initial Pitot Tube (-)	[+1]
Probe Length/Liner	3 Questa	K Factor	35.17	' Final Pitot Tube (-)	(+)

		·								
Maist: Cal	Sample	P. No. 1 Meter Vol.	Vel. Head	Orifice Diff,	Stack	, Total Meter	Hot Box	Iter Tare Exit	Pump	
No.	Time (min.)	Vm (ft³)	ΔP ("H₂O)	ΔH . ("H₂O)	Temp.,Ts (°F)	Temp., Tm (°F)	Temp. (°F)	Temp.	Vacuum ("Hg)	Other
1	0	121, 240	. DH	1,41	1345	90	239	65	1.0	
2	25	123,00	.035	1.23	1375	90	240	65	1.5	
3	5	124.65	.04	1,41	1395	<u>90</u>	245	65	10	
4	7.5	126.39	,035	1,23	1386	<u>70</u>	24.3	64	1.0	
5	iO	128.04	,035	1.23	1328	91	23C	64	1.0	
6	12.5	129.69	,03	1.06	1324	91	249	63	1.0	
7	15_	131.22	, 03	1,00	1329	91	257	63	1.0	<u></u>
8	17.5	132.72	, 03	1.06	1340	92	1264	62	1.0	
9	30	134,24	,03	1.06	1350	92	269	62	1.5	·
10	32.5	135.76	1035	1,23	1362	92	268	62	1.5	ļ ———
11	25	137,40	,63	1.0C	13/1	93	267	6/	1.5	<b> </b> -
12	27.5	138,91	.03	1.06	1385	93	265	61	1.5	<del> </del>
13	30	140.43	<u>~73</u>	1.06	1391	93	260	61	1.5	<b> </b> -
14	32.5	141.96	.03	1.06	1380	93	252	60	1.5	ļ
15 3	35	143.46	103	1.00	1370	93	248	GL	1.0	
16	37.5	144.97	,03	1.00	1352	9.3	1248	60	1.5	ļ <u>.</u>
17	40	146,49	.03	1.06	1344	94	1252	60	1.5	<del> </del>
18 6	1-12.5	148,00	,03	1.00	1347	94	257	60	1.5	
19	45	147.51	.03	1,00	1345	95	1266	60	1.5	<u> </u>
20	47.5	157.02	,03	1.06	1349	9.5	267	59	65	<del> </del>
21 9	50	152.52	103	1.06	1360	96	264	59	1.5	
22	555	154.04	,03	1.06	1361	96	202	60	4.5	ļ
23	55	155.55	,03	106	1363	96	1261	60	1.5	
24	\$7.5	157, io	,03	1.06	1370	96	260	60	1,0	
	(0	158.578	<u></u>	<u> </u>	<u> </u>			1		}

#### GAS ANALYSIS DATA FORM

Plant FOSTER'S PET Cremation:	Service
Unit Animal Crematory Incinerator	· .
Date 3/9/04	Sampling Location STacK
Sampling Time (24-hr Clock) 1135-1235	
Sample Type: Continuous 🗆 Integrated Bag 🇖	Grab □
Analytical Method	Ambient Temperature 68°F
Operator y1) &	

RUN →		1		2		3	Average		Molecular Weight of Stack
GAS ↓	Actual Reading	Net	Actual Reading	Net	Actual Reading	Net	Net Volume	Multiplier	Gas (Dry Basis) (Md)
CO <sub>2</sub>	4.5	4.5	4.5	4.5	4.5	4.5	4.5	.44	
O2 (NET IS ACTUAL O2 READING MINUS ACTUAL CO2 READING)	12.5	8,0	12.5	8,0	12.6	8,1	8.0	.32	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O <sub>2</sub> READING)								.28	
N₂ (NET IS 100 MINUS ACTUAL CO READING)					1. 5 1. 5			.28	
							TOTAL		

### GAS ANALYSIS DATA FORM

Plant FOSTer'S Pet Cremation Service							
Unit Animal Crematory Incinerator	Test No. 2						
Date 3/9/04	Sampling Location STeCK						
Sampling Time (24-hr Clock) 1302 - 1402							
Sample Type: Continuous 🗆 Integrated Bag. 💢	Grab □						
Analytical Method DYSAT	Ambient Temperature 74°/2						
Operator MG							

RUN →		 		2		3	Average		Molecular Weight of Stack
GAS ↓	Actual Reading	Net	Actual Reading	Net	Actual Reading	Net	Net Volume	Multiplier	Gas (Dry Basis) (Md)
CO <sub>2</sub>	4.5	4.5	4.5	4.5	4.5	4.5	4.5	.44	
O <sub>2</sub> (NET IS ACTUAL O <sub>2</sub> READING MINUS ACTUAL CO <sub>2</sub> READING)	14.5	10.0	14.5	10.0	14.5	10,0	10.0	.32	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O <sub>2</sub> READING)								.28	
N₂ (NET IS 100 MINUS ACTUAL CO READING)								.28	
							TOTAL		

#### GAS ANALYSIS DATA FORM

Plant FOSTER'S PET Cremati	on Scrvice
Unit Animah Crama Tory	Test No. 3
Date 3/9/04	Sampling Location STack
Sampling Time (24-hr Clock) 1425-1525	
Sample Type: Continuous 🗆 Integrated Bag 🛱	Grab □
Analytical Method OSSAT	Ambient Temperature 75°
Operator M G	

RUN →	. 1	1		2		3	Average		Molecular Weight of Stack
GAS ↓	Actual Reading	Net	Actual Reading	Net	Actual Reading	Net	Net Volume	Multiplier	Gas (Dry Basis) (Md)
CO <sub>2</sub>	5-5	5,5	5,5	5,5	5,5	5.5	5.5	.44	
O2 (NET IS ACTUAL O2 READING MINUS ACTUAL CO2 READING)	16.0	10.5	16.0	10.5	16.0	10.5	10.5	.32	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O <sub>2</sub> READING)								.28	
N₂ (NET IS 100 MINUS ACTUAL CO READING)								.28	
							TOTAL		

## SOUTHERN ENVIRONMENTAL SCIENCES, INC. NOZZLE CALIBRATION

Date: 3/9/04 by:

Nozzie ID	Run No.	D <sub>1</sub>	D <sub>2</sub>	D <sub>3</sub>	AD (inches)	D <sub>AVG</sub>
Quitz	1-3	.611	,611	a611	.000	1611

where:

 $D_1$ ,  $D_2$ ,  $D_3 =$ 

Nozzle diameter measured on a different

diameter (inches).

Tolerance = 0.001 inches

ΔD

Maximum difference in any two

measurements (inches).

Tolerance = 0.004 inches

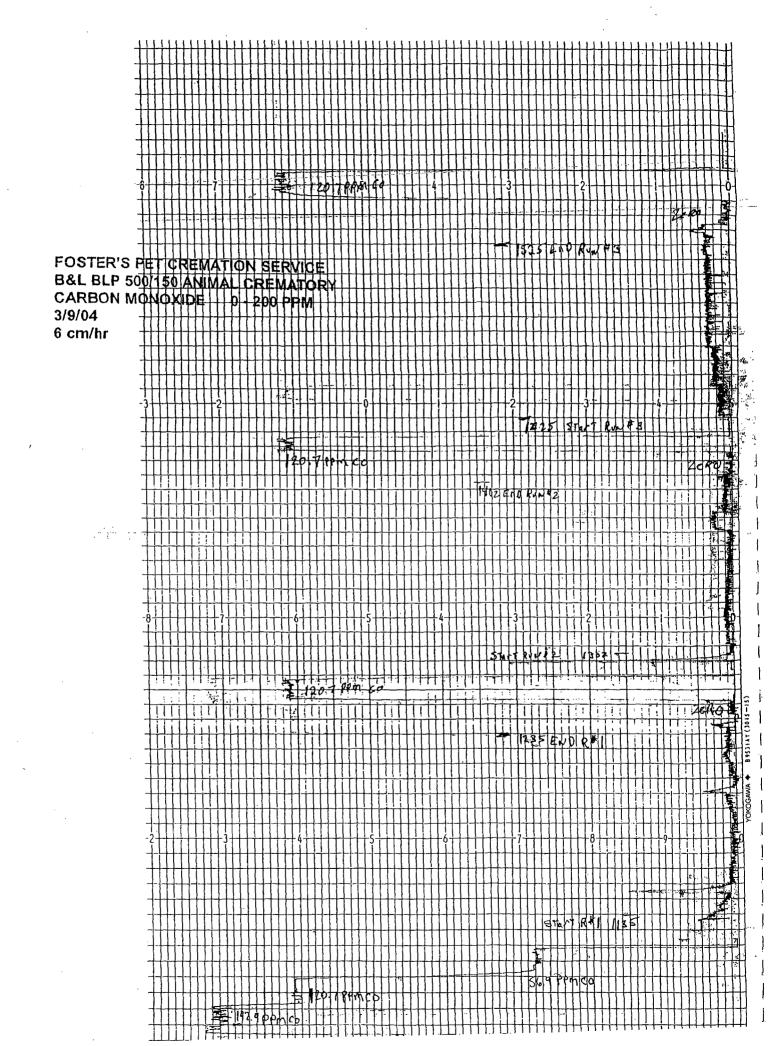
D

= Average of  $D_1, D_2, D_3$ 

#### SAMPLE POINT LOCATIONS

Company: Testers Rt Renation					
Source: An mel Clematery in cheinter					
Date: 3/9/04/					
Stack/Duct Dimensions: /5"					
Port Length: 3 <sup>1</sup>					
Points corrected for port length? Yes ☑ No □					
Sketch of Stack/Duct					

Point No.	Distance from Duct Wall (inches)
<del> </del>	3,5
2	4,2
3	5.1
14 5 6 7 8	6.2
5	7.5
6	9.4
7	14.6
8	K.5
	17.4
10	19.9 11.8
12	20:5
	2013
	<del></del>



#### DRY GAS METER CALIBRATION

Meter Box Number:

002

Barometric Pressure:

29.99

Date: 07/03/2003

Wet Test Meter No.:

P-576

Onlice	Gas	/alume	iem	eratura			
Agroneta Santa	Wet Test Merer	Liny Class Market	Vie Teg	Ery Cas Meter	Time		Delta H@
(Delta A) In 1420	0.4	EVI)	Seg.	CEST Deg F	(THETA)		in H201
0.50	5.000	5,155	76.0	86.5	12.15	0.988	1.641
1.00	5.000	5.196	76.0	91.0	8.88	0.987	1.738
1.50	10.000	10.428	76.0	93.0	14.28	0.986	1.680
2.00	10.000	10.470	75.5	95.0	12.50	0.985	1.707
3.00	10.000	10.489	75.0	97.0	10.43	0.985	1.773
4.00	10.000	10.485	75.0	98.0	9.15	0.985	1.816
						0.986	1.726

Delta H@ Acceptable Range Yi Acceptable Range

1.926 1.006

to to

1.526 0.966

$$Yi = \frac{Vw Pb (Td + 460)}{Vd (Pb+DeltaH/13.6) (Tw + 460)}$$

Where:

Vw = Gas Volume passing through the wet test meter, ft.^3.

Vd = Gas Volume passing through the dry gas meter, ft.^3.

Tw = Temperature of the gas in the wet test meter, deg F.

Tdi = Average temperature of the gas in the dry gas meter, deg F.

Delta H = Pressure differential across orifice, in. H20.

Yi = Ratio of accuracy of wet test meter to dry gas meter for each run.

Y = Average ratio of accuracy of wet test meter to dry gas meter for all three runs; tolerance = pretest Y = 1-0.05Y.

Pb = Barometric pressure, in. Hg

Theta = Time of calibration run, min.

#### POSTTEST DRY GAS METER CALIBRATION FORM

Meter Box Number:

002 \

Wet Test Meter No.:

P-576

Date: 03/24/2004

00. 00/21/200

Pretest Y:

0.986

Barometric Pressure:

30.38

Calibrated by:

TW

Manariae Sanna						Vecilia	
2.00	10.000	<b>译图</b> 例 5	71.5	78.0	12.57	in Ho.00	0.972
2.00	10.000	10.503	71.0	86.0	12.62	10.00	0.974
2.00	10.000	10.632	71.0	93.0	12.67	10.00	0.975
						Average	0.974

Acceptable Limits

0.937

to

1.035

Where:

Vw = Gas volume passing through the wet test meter, ft.^3.

Vd = Gas volume passing through the dry gas meter, ft.^3.

Tw = Temperature of the gas in the wet test meter, deg F.

Tdi = Temperature of the inlet gas of the dry gas meter, deg F.

Tdo = Temperature of the outlet gas of the dry gas meter, deg F.

Delta H = Pressure differential across orifice. in. H20.

Yi = Ratio of accuracy of wet test meter to dry gas meter for each run.

Y = Average ratio of accuracy of wet test meter to dry gas

meter for all three runs; tolerance = pretest Y =/- 0.05Y.

Pb = Barometric pressure, in. Hg

Theta = Time of calibration run, min.

#### THERMOMETER CALIBRATIONS

Referen	∴ a Wet Te	st Meter	Dry Ga	s Meter
	alalet 🗼	e Outlet	a a Inletar	Ciller :
DegF	Degr	Deg F	Ded F	Deg F
75.0	n/a	73.0	n/a	73.0
aDifference.	n/a	2.0	n/a	2.0

Quality Control Limits = +/- 5 Deg F

### TYPE S PITOT TUBE INSPECTION FORM

PITOT TUBE ID NUMBER	003INC				
INSPECTION DATE	03/31/03				
INSPECTED BY	T. Wilson				
PITOT FUBE ASSEMBLY LEVEL 7	YES NO				
PITOT TUBE OPENINGS DAMAGED?	YES (explain please)	(NO)			

ANGLE	MEASUREMENT	LIMITS
αΙ	. 2°	<10°
a2	3°	<10°
. b1	3°	<5°
b2	2°	<5°
Y	2°	
θ	3°	·
А	.290 inches	
$z = A \sin Y$	.010 inches	< 1/8 inch
$w = A \sin \theta$	.015inches	< 1/32 inch
Pa .	.145 inches	
Pb	.145 inches	
Dt	.190 inches	

COMMENTS:		; ;-		•
CALIBRATION REQUIRED	YES		N	0

### SOUTHERN ENVIRONMENTAL SCIENCES, INC. THERMOMETER CALIBRATIONS

Calibrated By/Date: T. Wilson 3/31/03

ALL TEMPERATURES ARE DEGREES RANKIN

Call	nated	by/Date	: I. VVIISO	11 3/3 1	/03	<del>, ;;</del>		<del></del>	<del></del>	ALL IEI	MPERATURES A	ARE DEGREES H	ANKIN		1
ļ.				CE BAT	TH	Тт	EPID WA	ŢER	BO.	ILING WA	ATER	<u> </u>	нот оп	·	<u> </u>
ID No.	Туре	Range	STD Therm	Temp	Deg or Diff	STD Therm	Temp	Deg or Diff	STD Therm	Temp	Deg or Diff	STD! Therm	Temp	Deg	or Diff
T1	PT	2000° F	495	496	0.2%	539	537	0.1%	672	670	0.2%	860	861	0.	3%
T2	PT	2000° F	495	497	0.2%	539	537	0.1%_	673	672	0,2%	870	872	0.	3%
ТЗ	PT	2000° F	495	497	0.2%	539	538	0.1%	673	.671	0.3%	870	872	О.	2%
T4	PT	2000° F	494	496	0.2%	539	538	0.1%	674	672	0.3%	863	864	0.	2%
T5	PT .	2000° F	494	496	0.2%	539	538	0.2%	672	670	0.2%	860	862	0.	2%
. T6	PT	2000° F	494	496	0.2%	539	537	0.3%	672	674	0.3%	852	854	0.	2%
17	PT	2000° F	495	497	0.2%	539	538	0.3%	673	671	0.2%	853	854	. 0.	3%
Т8	PT	2000° F	495	496	0.1%	539	537	0.2%	674	672	0.1%	864	865	0.	2%
Т9	PT	2000° F	495	497	0.1%	539	538	0.3%	673	671	. 0.1%	854	856	0.	3%
Lab 14	ВМ	. 212° F	494	495	1 0	538	535	1 °	672	673	2 °	•	•		
15	ВМ	250° F	494	495	1 °	536	535	1 °	672	672	2°	•		. 1	
. 16	ВМ	220° F	494	. 496	. 1 a	536	536	2°	672	672	3•	•		-	
<b>5S</b> 110	вм	220° F	494	496	1 •	540	539	2°	670	672	2°	•		<u> </u>	
ss300	PT	2000 °F	495	497	0.2%	.540	538	0.1%	674	672	0.2%	850	852	0.2	%
SS301	PT	2000° F.	495	497	0.2%	540	538	0.2%	672	670	0.1%	856	858	0.2	.%
ss306	PT	2000° F	495	496	0.2%	540	538	0.2%	672.	670	0.2%	856	858	0.2	<b>%</b>
2.5'PA	PT -	2000° F	495	496	0.2%	541	538	0.0%	673	672	. 0.2%	852	854	0.3	%
2.5'P8	PΤ	2000° F	. 495	497	0.2%	541	538	0.0%	672	674	0,3%	856	858	0.3	% .
3'P	PT	2000° F	495	497	0.2%	541	539	0.1%	673	675	0.2%	858	860	0.3	%
3'INC	PT	. 2000° F	494	496	0.1%	540	538	0.1%	676	678	0.2%	852	854	0.3	%
5'PA	PT	2000° F	494	496	0.3%	540	539	0.0%	672	674	0.3%	856	858	0.29	*
5.'PB	PT	2000° F	495	497	0.3%	540	538	0.1%	674	672	0.3%	856	858	0.39	6
5'PC	PT	2000° F	495	497	0.3%	540	538	0.2%	674	672	0.1%	856	858	0.39	6
5'VP	PT	2000° F	495	497	0.2%	541	540	0.2%	. 676	678	0,2%	856,	858	0.29	6
5'INC	PT	2000° F	494	496	0.3%	542	540	0.1%	674	676	0.1%	850	852	0.39	6
8:PA	PT -	2000° F	494	496	0.3%	541	538	0.0%	676	678	0.2%	856	858	0.2%	6
8'PB	PT	2000° F	494	495	0.3%	541	539	0.1%	676	678	0.3%	858	858	0.29	6
10'P	PT	2000° F	494	495	0.2%	541	539	0.0%	674	676	0.3%	854	856.	0.2%	6
	<del></del>		<del></del>	<del></del>	Her Impieses Thes	205	27.		F05.5			<del></del>		<u>_</u>	

Quality Control Limits: Impinger Thermometers# 2°F, Bimetalic Thermometers(Bm)# 5°F,Pyrometers/Thermocouples(PT)# 1,5%

### PRESSURE MEASUREMENT DEVICE CALIBRATION FORM

Device Type	Magnehelic	Calibration Date	04/01/2003
Range	025" H2O	Calibrated by	K. Roberts
Manufacturer	Dwyer	Reference Device	, Manometer
Serial No.	R991014CA18	Measurement Units	' H2O

Device Reading	Reference Device Reading	% Difference*
0	0	0.00
0.059	0.06	-1.67
0.119	0.12	-0.83
0.18	0.18	0.00
0.249	0.25	-0.40

<sup>\* %</sup> difference shall not exceed +/- 5%

1204 North Wheeler Street St. Plant City, Florida 33563 (813) 752-5014

#### **INSTRUMENT CALIBRATION**

TESTIDATAY	
TO MERCE !	03/09/2004
COMPANY	FOSTER'S PET CREMATION SERVICE
· isquecea	BLP 500/150 ANIMAL CREMATORY
EARWANEHER IN	CARBON MONOXIDE
TECHNICIAN	M. GIERKE

INSTRUMENT/DATA		
	## * MONITORY ###	F-WRECOEDERS.
MANUEACHURER	TECO	Yokogawa
- Votelino	48	
THE PART OF THE	48-27158-228	
PRANCE (PRM)	200	6CM/HR

CALIBRATION GASE		41.45.09.04.45.25.25.25.25.25.25.25.25.25.25.25.25.25	
SUPPLIER	AIR PRODUCTS	AIR PRODUCTS	AIR PRODUCTS
CYLINDER#	SG9170323	SX32489	SG9162702
CONC. (PPM)	56.9	120.7	142.4
EXPIRATION DATE	04/25/2004	01/06/2006	09/30/2006

ASSESSIONES STATE	* COBSERVED CONC	414 ACTUAL CONC.	Y RERGENTIDIES
	0 .	0	0.00
2 5	55.6	56.9	-0.65
		120.7	0.65
2.4	142	142.4	-0.20

Regression Output:

constant.		1.6234
- Statem of Yelest		1.9109
/R/Squaledi		1.0000
Not of Observations		4
Degrees of Preedom:		2
X Coefficients)	1.0058	
StdEtrof, Coet	0.0029	



ir Products and Chemicals, Inc. \* 12722 S. Wentworth Avenue, Chicago, IL 60628

ISO CERTIFICATION: 9002

## E OF ANALYSIS: EPA PROTOCOL GAS ST

PERFORMED ACCORDING TO EPA TRACEABILITY PROTOCOL FOR ASSAY AND CERTIFICATION OF GASEOUS CALIBRATION STANDARDS (PROCEDURE #G1)

istomer: 851 -1

.PCI-LARGO

900 118TH AVENUE NORTH

ARGO

FL 33773-

Order No: CSS704108-01

Batch No: 86181785

PO:

Release:

Cylinder No:

SG9170323BAL

Bar Code No:

FHK790

Cylinder Pressure\*: 2000 psig

Certification Date: 04/25/2001

Expiration Date:

04/25/2004

CERTIFIED CO	NCENTRATION	REFERENCE STANDARDS			ANALYTICAL INSTRUMENTATION			
6	Certified	Cylinder	Standard	Standard	instrument	Serial	Last	Measurement
Component	Concentration	Number	Type	Concentration	Make/Model	Number	Calibration	Principal
CARBON MONOXIDE	56.9±.60 PPM	SG9161497BAL .	NTRM 81679	99.90 PPM	HORIBA VIA-510	405079	04/01/01	NON DISPERSIVE INFRARED

11 TROGEN

Balance Gas

\* STANDARD SHOULD NOT BE USED BELOW 150 PSIG

EPA PROTOCOL GAS MIXTURE : CARBON MONOXIDE IN NITROGEN To reorder this mixture please use Mix ID: 27578

alyst: SUZANNE HAUTER 3921)

Approved By:	anes	recos	ļ
		lamaa	1



Alrgas Specialty Gases
12722 South Wentworth Avenue
Chicago, IL 60628
773.785.3000 Fax: 773.785.1928
www.sirgas.com

### Certificate of Analysis: E.P.A. Protocol Gas Mixture

Certification performed in accordance with "EPA Traceability Protocol (Sept.1997)" using assay procedures listed.

			·····	•						
Cylinder No:	SX32489	0	rder No:	157779-00						
Certification Date:	01/6/2003	E	xpiration Date:	-	01/6/2006					
Cylinder Pressure:	2000	- P	art No:	•	E02NI99E15A0700					
*Do not use cylinder below	150 psig.	<del>-</del>		•						
	Certified	Unit of		·	Analytical					
Component	Concentration	<u>Measure</u>	Accuracy	<u>Procedure</u>	<u>Principle</u>					
Carbon Monoxide	120.7	PPM	1%	G-1	NDIR					
Nitrogen	Balance	·								
Nox	7.									
(Reference Value Only)										
Reference Standard Information										
Туре	Component		Concentration	<u>Unit</u>	Cylinder Number					
NTRM	Carbon Monoxide		244.7	PPM	SG9159519BAL					

#### Analytical Data

Component 1		Carbon Monoxide				
1st Analysis Date:		12/30/2002				
	Zero Zero Zero	0.000 0.000	Cand Cand Cand	120:700 120:700 120:700	Ref Ref Ref	244,800 244,800 244,800
2nd Analysis Date:		01/06/03				·
	Zero	0.000	Cand	120.800	Ref	244.800
	Zero Zero	0.000	Cand Cand	120.800 120.900	Ref Ref	244.800 244.700

Analyzed by:

Approved by: D. Jack

Alrgas Specialty Gases 12722 South Wentworth Avenue Chicago, IL 60628 773.785.3000 Fax: 773.785.1928 www.airgas.com

### Certificate of Analysis EPA Protocol Gas Mixture

Cylinder No:

SG9162702BAL

Reference Number:

54-ST9736-000

Cylinder Pressure:

2,013 psig

Expiration Date:

09/30/2006

Certification Date:

09/30/2003

Laboratory:

ASG - Chicago - IL

#### **Certified Concentrations**

Component	Concentration Accuracy	Analytical Principle	Procedure
Carbon Monoxide	142.4 PPM +/- 1%	NDIR	G1
Nitrogen	Balance		

Certification performed in accordance with "EPA Traceability Protocol (Sept. 1997)" using the assay procedures listed. Analytical Methodology does not require correction for analytical interferences.

Notes:

Do not use cylinder below 150 psig.

Approved for Release

Reference Standard Information

Type NTRM Component

Carbon Monoxide

Cyl. Number SG9159474BAL Concentration 244.7 PPM

Analytical Results

1st Component

Carbon Monoxide

1st	Analysis D	ate:	09	9/22	/2003		
R	244.7	S	142.3	Z	0.0000	Conc	142.4 PPM
S	142.4	Z	0.0000	R	244.7	Conc	142.3 PPM
Z	0.0000	R	244.7	S	142.4	Conc	142.4 PPM
						AVG:	142.4 PPM
2nd	d Analysis [	Date:	0	9/30	/2003		
R	244.7	S	142.5	Z	0.0000	Conc	142.4 PPM
S	142.4	Z	0.0000	R	244.7	Conc	142.5 PPM
Z	0.0000	R	244.7	S	142.5	Conc	142.5 PPM
						AVG:	142 5 DDM

#### CO EMISSION TEST CALCULATIONS

COMPANY: FOSTER'S PET CREMATION-SERVICE SOURCE: B&L BLP 500/150 ANIMAL CREMATORY

TEST DATE: 03/09/2004

Data analyst: MG

		Average							
	ÇQ.	02	CO Stack @ 7% O2 Flowrate			Emissions	Emissions		
Run No.	(PPM)	(%)	(PPM)	(dșefm)	mg/m3	lbs/ft3	lbs/hr		
1	3.08	8.0	3.3	457	3.6	2.24E-007	0.006		
2	2.25	10.0	2.9	482	2.6	1.64E-007	0.005		
3	5.0	10.5	6.7	501	5.8	3.63E-007	0.011		
Averages	3.44	9.5	4.3	480	4.0	2.50E-007	0.007		

FORMULAS:

 $CO @ 7\% O2 = Actual CO \times (14/(21-\%02))$ 

mg/m3 = ppm x .041573 x molecular wt.

 $\frac{\text{mg/m3}}{35.31 \text{ ft}^3/\text{m}^3 \times 1000 \text{mg/g} \times 453.59 \text{ g/lb}}$ 

lb/hr = lb/ft3 x flowrate x 60 min/hr

where:

Pstd =

29.92 "Hg

Tstd =

528 deg R

Molecular Weight of CO =

28

#### **EMISSIONS TEST CALCULATIONS**

Plant:

FOSTER'S PET CREMATION SERVICE

Unit: Run No: ANIMAL CREMATORY INCINERATOR

2

103.6

Test Date:

03/09/2004

Data Input By: DW\_

	<del></del>									<del></del>	
Pbar = (Pbar a =	t barom.) - (El 30.14	ev. diff. barom. -	to manor		/100) 0.1/100)	=	<u> 30.14</u>				
				·	·						
Pm = Pbar_+	Delta H =		30.14	+	1.041 13.6	=	<u>30,22</u>				
Vm(std) = (Vm	r) x (Y) x (ref T)	d,deg R) x (Pn m,deg R) x (Ps	<u>n)</u> std)								
<b>**</b>	36.308	<b>x</b>	0.986	×	<u>528</u> 553.7	х х	30.22 29.92	=	<u>34.476</u>		
Vw(std) =	Vlc x (.04715	) =	144.1	x	0.04715	=	<u>6.794</u>	:			
βws =	<u>Vw(std)</u> w(std) + Vm(s	td)	=	6.794	6.794	34.476	. <sup>=</sup>	<u>0.165</u>			
βws @ satura 1 - Bws =	ntion = 0.835	0.99	ţ	JSE LOWE	ER BWS						
	002) + .32(%0 14 x <u>ssume</u>	02) + .28(%N2 4.5 <b>29.12</b>		32 x	10	+	0.28	78			
Ms = Md(1-Bv =	ws) + 18(Bws) <u>27.29</u>	=	29.12	•	0.835	+	18	*	0.165		
Ps = Pbar + <u>(</u>	Pg, in. H2O) : 13.6	a.	30.14	+	-0.01 13.6	_ =	<u>30.14</u>				
Vs ≈ 85.49 x : = =	(Cp) x (avg sq 85.49 <u>18,68</u>	rt delta P) x sq x	rt[(Ts,~R 0.84	)/(Ps)(Ms)] x		x sqrt	1827.1	I	30.14	×	27.29
An = [( Nozzle	e diam, in./12) 4	^2 x 3.14159]			0.611	/12)^2 ×	c 3.14159]	Ξ	0.00204		
%I = (.09 (Ps) x (	9450) x (Ts,de Vs) x (An) x (S	g R) x (Vm(std ample Time) x	) (1-Bws)								
Ξ	0.0945 30.14	х х	1827.1 18.68	X X	34.476 0.0020361	×	60	X	0.835		

#### **EMISSIONS TEST CALCULATIONS**

Plant: Unit:

FOSTER'S PET CREMATION SERVICE

**ANIMAL CREMATORY INCINERATOR** 

Test Date: Data input By: 03/09/2004

DW

Run No:

2

As = (Stack Diam., ft.)^2 x 3.14 1.5 )^2 x 3.14 1.77

As.eff = As x (total No. pts.-No. neg. pts.) 1.77 (Total No. pts.)

Q = 60(As,eff)(Vs) =

60

1.77

18.68

x

1,981

30.139265 (Q) x (Tstd) x (Ps) x (1-B 1980.505 528 0.83537 1827.125 29.92

= <u>482</u>

 $Cs = (.01543) \times (mn, mg)$ 

0.00497 0.01543 11.1 34.4759

Vm(std)

PMR = (Cs)(Qstd)(67000

(Ts,degR) x (Pstd)

481.60559 x 60 0.0050 7000

0.02

Emissions calculations in emissions test summary may differ slightly from example calculations due to rounding of some numbers in example.

### Southern Environmental Sciences, Inc.

1204 North Wheeler Street ☐ Plant City, Florida 33566-2354 ☐ (813) 752-5014

## NOMENCLATURE USED IN STACK SAMPLING CALCULATIONS

 $A_n$  = Cross-sectional area of nozzle,  $ft^2$ 

 $A_a$  = Cross-sectional area of stack,  $ft^2$ 

B<sub>ws</sub> = Water vapor in gas stream, proportion by volume

 $C_p$  = Pitot coefficient

C<sub>s</sub> = Pollutant concentration, gr/DSCF

F<sub>d</sub> = Ratio of gas generated to heat value of fuel, DSCF/mm BTU

 $\Delta H$  = Average pressure differential across orifice, in.  $H_2O$ 

%1 = Isokinetic variation, %

 $M_d$  = Molecular weight of dry gas

 $M_n$  = Total amount of pollutant collected, mg

 $M_s$  = Molecular weight of stack gas

N = Normality of barium perchlorate titrant

 $\int \Delta P_{avg} = Average$  of the square roots of the velocity heads

 $P_{bar}$  = Barometric pressure at the sampling site, in. Hg

 $P_g$  = Stack gas static pressure, in.  $H_2O$ 

 $P_m = Absolute pressure at the dry gas meter, in. Hg$ 

P<sub>s</sub> = Absolute stack pressure, in. Hg

PMR = Pollutant mass rate, lb/hr

P<sub>std</sub> = Standard absolute pressure, 29.92 in. Hg

 $\theta$  = Total sampling time, minutes

### Southern Environmental Sciences, Inc.

1204 North Wheeler Street □ Plant City, Florida 33566-2354 □ (813) 752-5014

## NOMENCLATURE USED IN STACK SAMPLING CALCULATIONS

(Continued)

Q = Stack gas flowrate, ACFM

 $O_{end}$  = Stack gas flowrate, DSCFM

 $T_m$  = Absolute average meter temperature,  ${}^{\circ}R$ 

T<sub>s</sub> = Absolute average stack gas temperature, °R

T<sub>std</sub> = Standard absolute temperature, 528 °R

 $V_a = Volume of sample aliquot titrated, ml$ 

V<sub>le</sub> = Liquid collected in impingers and silica gel, grams

 $V_m$  = Sample volume at meter conditions, DCF

 $V_{m(std)}$  = Sample volume at standard conditions, DSCF

 $V_s$  = Stack gas velocity, ft/sec

 $V_{soln}$  = Total volume of solution, ml

 $V_t$  = Volume of barium perchlorate titrant used for the sample, ml

 $V_{tb}$  = Volume of barium perchlorate titrant used for the blank, ml

 $V_{wlstdl}$  = Volume of water vapor in sample corrected to standard conditions, SCF

Y = Dry gas meter calibration factor

13.6 = Specific gravity of mercury

right from your home or office at usps.com/pickup to usps.com/postageonline RMLY

Flat Rate

Visit us at usps.com

Mailing Envelope For Domestic and International Use



27200 JONES LOOP Rd. PUNTA GORDA, FE. 33982

From:/Expéditeur: PET HAVEN CEMETERY

To:/Destinataire:

FDEP RECEIPTS P. O. Box 3070 TALLAHASSEE, FL. 32315-3070

Country of Destination:/Pays de destination:

USA