	KC IND DAILY QUALITY CONI	USTRIES, LLC. FROL AND PRODUCTIC	DN LOG	
DATE: <u>17/1/11</u>	LOT #: <u> -335</u>	r (SFS	OR PFS PRODUCTION	N [circle one]
A OPERATOR:	BSON	SHI	FT:	
PRODUCT DRYING	START TIME: [* defined as the time period	<u>OUNO</u> I that product passes throug	STOP TIME:	125 le
	START TIME:		STOP TIME:	
	START TIME:		STOP TIME:	
		TIME 1	TIME 2	TIME 3
1. FLOWS ON TIME		0617		
2. FILTER START TIME		OLMO	<u></u>	
3. FLOWS OFF TIME		1245		
4. SCREWS DOWN TIME		250		
5. TIME	<u></u>	0740	0940	1140
6. BURNER EXIT TEMP		1.320'	17400	1.308
7. DRYER EXIT TEMP		347"	3540	.343°
8. VENT FAN AMPS		74	T4	24
9. DRAFT FAN AMPS			70	
10. CHLORIDES		40	_36	36
DOWN TIMES AND REASON	S:			
RAW MATERIALS USAGE				
TANK NUMBER:			<u>KCL</u>	
BEGIN OUTAGE :	_3'		\leq $=$	
END OUTAGE:	5'4"		_ _	
USAGE:	28"			
NUMBER OF LIQUID BRINE TR	UCKS UNLOADED	0		
NUMBER OF SALT TRUCKS	UNLOADED:	1		
NUMBER OF ACID TRUCKS	UNLOADED:	2		
NUMBER OF ACID RAILCAF	RS UNLOADED:	0		
NUMBER OF KCL RAILCAR		0		
TIME OF BATCHING PETRO	•	<u>7700 00</u> 11/20/11 1 13 14/1		
PETRO USED IN BATCHING		11386		

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REMARKS:

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DATE: $2 - 1 - 11$ LOT #:	KII-335	SFS OR PFS PRODUCTION [circle one]				
BOPERATOR:	· · · · · · · · · · · · · · · · · · ·		T: j st			
		SAMPLE	SAMPLE	SAMPLE		
1. TIME		0740	0940	1140		
2. PRODUCTION RATE Start plant at 105 tpd and go to 120- tpd once - 325 < 10%	[tpd]	120	120	120		
3. ACID [FSA] FLOW	[gpm]	53.4	53.4	53.7		
4. ACID [FSA] SPECIFIC GRAVITY		1217	1217	1217		
5. ACID [FSA] STRENGTH	%	24.500	24.370	24.370		
6. KC L/SALT BRINE FLOW	[gpm]	49.0	49.1	and the second s		
7. KCL /SALT BRINE SPECIFIC GRAVITY	Lor	1200	1200	1200		
8. COLOR OF BRINE		White	CLEAR	CLEAR		
[white, yellow, tan, brown]						
9. COLOR OF ACID		yellow	yellow	Yellow		
	[F]	•	· · ·			
10. REACTOR NO. 1 TEMP [PFS ONLY] Maintain between 110 and 140 degrees	[[]]					
11. DRYER TEMPERATURE Maintain between 310 and 350 degrees	[F]	<u>377°</u>	356	347		
12. VACUUM READING	["Hg]	12.5	12.0	13.0		
Maintain between 12 and 18 13. PRODUCT TEMPERATURE	[F]	251	1870	264		
14. VENTURI SCRUBBER WATER FLOW RAT		50	50	50		
MAINTAIN BETWEEN 50 AND 55 gpm	- Lor]					
15. VENTURI SCRUBBER AIR PRESSURE AT	INLET ["H20"]	10	10			
[POINT A] 16. VENTURI SCRUBBER AIR PRESSURE AT [POINT B]	OUTLET ["H20"]	2	_2	_2		
[POINT B] 17. VENTURI SCRUBBER DIFFERENTIAL PRI	ESSURE ["H2O"]	8	8	8		
[POINT A-B] Maintain between 8 and 14 inches of water	r 1	LI 1	110	112		
18. WET SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 42 AND 47 gpm	[gpm]	<u> </u>	-42	_72		
19. WET SCRUBBER WATER PRESSURE MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZL	[psig] E	_21	21	<u>_a</u> [
20. WET SCRUBBER AIR PRESSURE AT INLE [POINT B]		2	2	_2		
21. WET SCRUBBER AIR PRESSURE AT OUT	LET ["H20"]	.5	:5	<u> </u>		
[POINT C] 22. WET SCRUBBER DIFFERENTIAL PRESSU	RE ["H20"]	1.5	1.5	1.5		
[POINT B-C] Maintain between 1.0 and 4.5 inches of water						
21. FRESH WATER TO REACTOR	 [gpm]	X	X	×		
22. PETRO TO PRODUCT ON FILTER	[gpm]	3.5	3.5	3.5		
23. RINSE WATER TO PRODUCT ON FILTER	[gpm]	7.0	7.D	7.0		
PRODUCT SCREEN ANALYSIS		SAMPLE	SAMPLE	SAMPLE		
+60		35 1,20	31 .20	. 8		
+100	[Should be less than 20]	7.9 6.8	5.8 5.1	7 5.1		
+200	[Should be less than 70]	47.8 51.	3 49.9 52.			
+325	[Should be less than 30]	26.5 28.				
-325	[Should be less than 10]	16.2 12.				
** If you are not able to maintain the				ately.		
Condition of Y-Strainer?:	Did	you have to Clean it?) 			
REMARKS:						

1×n - √m€ ^{**}	DAILY Q	KC I UALITY CO	INDUSTRII		CTION LO	DG	
DATE: <u>[2-1-()</u>	LOT #:	<u>KII-3</u>	35		SFS OR I	PFS PRODUCT	ION [circle one]
A OPERATOR: <u>CHAN</u>	JCEY				SHIFT:	2nd	
PRODUCT DRYING	START T [* defined		<u>1550</u> eriod that pro	oduct passes	through the	STOP TIME: drying column]	2140
	START T	IME:	The same of the	n a la suite de la companya de la co		STOP TIME:	
	START T	IME:		na iya ka mana ka	_	STOP TIME:	
				TIME 1		TIME 2	TIME 3
1. FLOWS ON TIME				1532			Parameter The summer and a summer and the sum of the sum
2. FILTER START TIME				1550	Lin .		ALTERNATIVE CONTRACTOR AND STREAM OF A
3. FLOWS OFF TIME				2120	-		********
4. SCREWS DOWN TIME				2140	-		aliana ya ku nya ku
5. TIME				1650_		1850	2050
6. BURNER EXIT TEMP				MA		MA	MA
7. DRYER EXIT TEMP				361		369	345
8. VENT FAN AMPS				25		25	25
9. DRAFT FAN AMPS				70	Nation 1	48	0
10. CHLORIDES				31	-	25	<u></u>
DOWN TIMES AND REASONS:							
RAW MATERIALS USAGE			,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	n in a stand of the second	an de la seconda da la seconda de la sec		n, a gran i frankt i na stalan ski kan kan sa
TANK NUMBER:	3	<u>FSA</u>	Naraphile Albandiana ana atsar ats		and the second secon	<u>KCL</u>	
BEGIN OUTAGE:	5'4"		9759		a finn a shi ka finn a finn a san ar af a suar		
END OUTAGE:	7'1"						
USAGE:	21"		*****		\angle	naay entran	۲۰۰۰ ۲۰۰۰ ۲۰۰۰ ۲۰۰۰ ۲۰۰۰ ۲۰۰۰ ۲۰۰۰ ۲۰
NUMBER OF LIQUID BRINE TRU	CKS UNLOA	DED	Ø				
NUMBER OF SALT TRUCKS U	NLOADED						
NUMBER OF ACID TRUCKS U	NLOADED:	:					
NUMBER OF ACID RAILCARS	UNLOADE	D:	Ø	NDC-4			
NUMBER OF KCL RAILCARS	UNLOADEI):	Ŀ				
TIME OF BATCHING PETRO					104		
PETRO USED IN BATCHING			an a	BATC	NED,		

REMARKS:

DATE: <u>12-1-11</u> LOT #: <u>k/1</u> B OPERATOR: Conder				
Javeco		JAMPLE	SAMPLE	SAMPLE
1. TIME		11650	1950	2053
2. PRODUCTION RATE	[tpd]	120	100	100
Start plant at 105 tpd and go to 120- tpd once - 325 < 10% 3. ACID [FSA] FLOW	[gpm]	53.6	43.5	43
4. ACID [FSA] SPECIFIC GRAVITY	Lep1	1.216	1214	1214
5. ACID [FSA] STRENGTH	%	04.25	24.25	2425
6. KCL/SALT BRINE FLOW	[gpm]	50	38	37
7. KCL/SALT BRINE SPECIFIC GRAVITY	1811	1.201-1.2	20 - 1197	1193
8. COLOR OF BRINE		white	white	white
(white, yellow, tan, brown)		11		· · · lla -
9. COLOR OF ACID (white, yellow, tan, brown)		_ Yp lland	_yeller	- Yellow
10. REACTOR NO. 1 TEMP [PFS ONLY] Maintain between 110 and 140 degrees	[F]			
11. DRYER TEMPERATURE Maintain between 310 and 350 degrees	[F]	358	363	343
12. VACUUM READING	["Hg]	14	_14_	
Maintain between 12 and 18 13. PRODUCT TEMPERATURE	[F]	271	268	275
14. VENTURI SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 50 AND 55 gpm	[gpm]	50	_50	57
15. VENTURI SCRUBBER AIR PRESSURE AT INLET	["H20"]	10	p	10
[POINT A] 16. VENTURI SCRUBBER AIR PRESSURE AT OUTL. [POINT B]	et ["H20"]	2	2	2
17. VENTURI SCRUBBER DIFFERENTIAL PRESSUR	E ["H20"]	8		2
[POINT A-B] Maintain between 8 and 14 inches of water 18. WET SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 42 AND 47 gpm	[gpm]	42	42	42
19. WET SCRUBBER WATER PRESSURE MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	[psig]	21	21	22
20. WET SCRUBBER AIR PRESSURE AT INLET [POINT B]	["H20"]	2	_2	2
21. WET SCRUBBER AIR PRESSURE AT OUTLET [POINT C]	["H2O"]	.5	<u>~5</u>	.5
22. WET SCRUBBER DIFFERENTIAL PRESSURE	["H2O"]	1.5	1.5	1.5
[POINT B-C] Maintain between 1.0 and 4.5 inches of water				
21. FRESH WATER TO REACTOR	[gpm]			
22. PETRO TO PRODUCT ON FILTER	[gpm]	4.0	4.0	4.0
23. RINSE WATER TO PRODUCT ON FILTER	[gpm]	7.0 175	0 7,0	7.7
PRODUCT SCREEN ANALYSIS		SAMPLE 19	SAMPLE	SAMPLE
+60		217 012	- 13 11	
-	ld be less than 20]	<u>6.3</u> 7.6 57.2 58.		7.4
	Id be less than 70] Id be less than 30]	$\frac{57.2}{13.8}$ 12.		
•	ild be less than 10]	13.5 11		
-	-			the second s
** If you are not able to maintain the above p		you have to Clean it		matery.
Condition of Y-Strainer?: 01/2		you have to Clean h	t? <u>A</u> 9	

х. . фо	KC I DAILY QUALITY CO	NDUSTRIES, LLC.	DICTION L	ne	Ø
DATE: <u>///////</u>		334		PFS PRODUCTIO	N [circle one]
A OPERATOR: DOBS	ons		SHIFT:	151	
PRODUCT DRYING	START TIME:	0770		STOP TIME:	1429
	[* defined as the time per	riod that product passe	es through the		
	START TIME:			STOP TIME:	
	START TIME:			STOP TIME:	
		TIME 1		TIME 2	TIME 3
1. FLOWS ON TIME		045	5		
2. FILTER START TIME		07	70		
3. FLOWS OFF TIME		1415			
4. SCREWS DOWN TIME		1429			
5. TIME		0 Be	70	1020	1720
6. BURNER EXIT TEMP		_N/I	9-1	NIA	in la
7. DRYER EXIT TEMP		262	- 6 	.268°	370°
8. VENT FAN AMPS		24		21	24
9. DRAFT FAN AMPS		70			70
10. CHLORIDES		54		213	29
DOWN TIMES AND REASONS:					
RAW MATERIALS USAGE					n
TANK NUMBER:	<u> </u>		~	<u>KCL</u>	
BEGIN OUTAGE:	7'1"				
END OUTAGE:	919"				
USAGE:	32 "				
NUMBER OF LIQUID BRINE TRU	CKS UNLOADED				
NUMBER OF SALT TRUCKS U	NLOADED:	Ø			
NUMBER OF ACID TRUCKS U	NLOADED:	2			
NUMBER OF ACID RAILCARS	UNLOADED:	0			
NUMBER OF KCL RAILCARS	UNLOADED:	0			
TIME OF BATCHING PETRO		11spin	1 Anta	1/87	
PETRO USED IN BATCHING		HINN	V BAEC.	(1,1,1)	
REMARKS:					

SHAKER SCREEN CONDITION AFTER LOADING TRAILER: PRODUCTION TRAILER INTERNAL CONDITION AFTER UNLOADING:

•

DATE: <u>[2-2-] </u> LOT #: _ B OPERATOR:Sy /1A	K11-336	SFS OR PFS PRODUCTION [circle one] SHIFT: / ⁵⁷			
		SAMPLE	SAMPLE	SAMPLE	
1. TIME		0820	1020	1220	
2. PRODUCTION RATE	[tpd]	120	12p	120	
Start plant at 105 tod and go to 120- tod once - 325 < 10% 3. ACID [FSA] FLOW	[gpm]	53.5	53.5	53.5	
4. ACID [FSA] SPECIFIC GRAVITY	[6]	1217	1217	1217	
5. ACID [FSA] STRENGTH	%	24.370	24.39	24.3 %	
6. KCL /SALT BRINE FLOW	[gpm]	48.8	46.4	48.2	
7. KCL /SALT BRINE SPECIFIC GRAVITY	LOF1	1202	1200	1200	
8. COLOR OF BRINE		CIEAR	CLEAR	CLEAR	
[white, yellow, tan, brown]		vatle.	Yellow	valla.)	
9. COLOR OF ACID [white, yellow, tan, brown]		yellow	Jenow	yendu	
10. REACTOR NO. 1 TEMP [PFS ONLY] Maintain between 110 and 140 degrees	[F]	<u> X </u>	_ <u>X</u>	<u>_X</u>	
11. DRYER TEMPERATURE Maintain between 310 and 350 degrees	[F]	<u>377</u>	368	359	
12. VACUUM READING	["Hg]	12.5	12.5	14.0	
Maintain between 12 and 18 13. PRODUCT TEMPERATURE	[F]	2770	2.57"	2107	
14. VENTURI SCRUBBER WATER FLOW RATE		50	50	<u>SD</u>	
MAINTAIN BETWEEN 50 AND 55 gpm 15. VENTURI SCRUBBER AIR PRESSURE AT IN	1LET ["H20"]	lp	10	10	
[POINT A]		·	2	<u></u>	
16. VENTURI SCRUBBER AIR PRESSURE AT O [POINT B]	UTLET ["H20"]		<u> </u>	<u> </u>	
17. VENTURI SCRUBBER DIFFERENTIAL PRES [POINT A-B] Maintain between 8 and 14 inches of water	SSURE ["H20"]	8			
18. WET SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 42 AND 47 gpm	[gpm]	_42	42	42	
19. WET SCRUBBER WATER PRESSURE MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	[psig]	_21	21	21	
20. WET SCRUBBER AIR PRESSURE AT INLET [POINT B]	["H2 0"]	_2	_2	_2	
21. WET SCRUBBER AIR PRESSURE AT OUTLI [POINT C]	ET ["H2O"]	<u></u>	5	<u>, 5</u>	
22. WET SCRUBBER DIFFERENTIAL PRESSUR [POINT B-C] Maintain between 1.0 and 4.5 inches of water	E ["H20"]	1.5		1.5	
21. FRESH WATER TO REACTOR	[gpm]	<u> </u>	<u> </u>	X	
22. PETRO TO PRODUCT ON FILTER	[gpm]	3.5	3.5	3.5	
23. RINSE WATER TO PRODUCT ON FILTER	[gpm]	7.0	7.0	7.0	
PRODUCT SCREEN ANALYSIS		SAMPLE	SAMPLE	SAMPLE	
+60	at 111 1	<u>·12 1</u>	.12/	.15	
-	Should be less than 20]	5.6 7.		5.7	
-	Should be less than 70] Should be less than 30]		4.4 53.0	48.8	
•	Should be less than 10]		7.4 26.4	28.7	
** If you are not able to maintain the al	-	يبتز بمتاليسة أسببين مسببا المتصحين			
Condition of Y-Strainer?:		you have to Clean i		nately.	
REMARKS.					

REMARKS:

		DAILY Q		INDUSTRI ONTROL A		UCTION LO	DG	
DATE: 17/5/	2	LOT #:	<u>_K11-</u>	339		SFS OR I	PFS PRODUCTIO	N [circle one]
A OPERATOR:	DORS	on)				SHIFT:	137	۵
PRODUCT DRYING		START TI [* defined a		 Deriod that pr	ZD oduct passes	through the	STOP TIME:	1335
		START TI	ME:			_	STOP TIME:	
		START TI	ME:	<u></u>			STOP TIME:	
					TIME 1	<i>F</i> -1	TIME 2	TIME 3
 FLOWS ON TIME FILTER START TIME 	AT:				013			
3. FLOWS OFF TIME	VID.				1315			ter and the second s
4. SCREWS DOWN T	IME				13.35			
5. TIME					DESI	2	1020	0551
6. BURNER EXIT TEN					<u></u>	1	NIA	N/X
7. DRYER EXIT TEM	P				325		3760	345
8. VENT FAN AMPS	1				- 27		<u>-35</u>	- 23
9. DRAFT FAN AMPS	•				<u></u>			10
10. CHLORIDES					_//_		3	
DOWN TIMES AND	REASONS: Product	*	STARTA	D Fili	TEXING	litte	DUE TO	FILTRATE
RAW MATERIALS U	JSAGE							
TANK NU	MBER:	2	<u>FSA</u>	<u></u>			<u>KCL</u>	
BEGIN OU	UTAGE:	2' 1/z"		· · · · · · · · · · · · · · · · · · ·		<u> </u>		
END OUT	AGE:	4'4				<u></u>		
USAGE:		29 1	, (1 ,					
NUMBER OF LIQUID NUMBER OF SALT NUMBER OF ACID NUMBER OF ACID NUMBER OF KCL R TIME OF BATCHING PETRO USED IN BA	TRUCKS UN TRUCKS UN RAILCARS AILCARS U G PETRO	NLOADED: NLOADED: UNLOADEI);		- - - -Bntch	ED Al.	Kendy	
DEMADES.								

REMARKS:

BOPERATOR: SYLVIA		39 SFS OR PFS PRODUCTION [circle of					
			T: 151				
sa <mark>ttan funktiona</mark> n and an		 SAMPLE	SAMPLE	SAMPLE			
1. TIME		0825	1025	1225			
2. PRODUCTION RATE Start plant at 105 tpd and go to 120- tpd once - 325 < 10%	[tpd]	120	120	120			
3. ACID [FSA] FLOW	[gpm]	55.6	55.6	50.2			
4. ACID [FSA] SPECIFIC GRAVITY		1210	1211	1211			
5. ACID [FSA] STRENGTH	%	23.1090	23.75 20	Q3.7.5 %			
6. KCL/SALT BRINE FLOW	[gpm]	49.1	47.3	44.4			
7. KCL/SALT BRINE SPECIFIC GRAVITY	LorJ	1200	1200	1198			
8. COLOR OF BRINE		CLEAR	Clent	CLEAR			
[white, yellow, tan, brown]			<u> </u>				
9. COLOR OF ACID		YELLOW	yellow	yellow_			
[white, yellow, tan, brown] 10. REACTOR NO. 1 TEMP [PFS ONLY]	[F]	X	X	X			
Maintain between 110 and 140 degrees	L- 1						
11. DRYER TEMPERATURE Maintain between 310 and 350 degrees	[F]	21010	376	364			
12. VACUUM READING	["Hg]	14.0	14.D	14.0			
Maintain between 12 and 18 13. PRODUCT TEMPERATURE	[F]	1850	2670	21090			
14. VENTURI SCRUBBER WATER FLOW RATE	[gpm]	.50	50	50			
MAINTAIN BETWEEN 50 AND 55 gpm	[8]]						
15. VENTURI SCRUBBER AIR PRESSURE AT INLET [POINT A]	["H20"]	10	_1D	<u>fo</u>			
16. VENTURI SCRUBBER AIR PRESSURE AT OUTLET [POINT B]	["H20"]	<u>_2</u>	_2				
17. VENTURI SCRUBBER DIFFERENTIAL PRESSURE [POINT A-B] Maintain between 8 and 14 inches of water	["H20"]			<u>-</u> 8			
18. WET SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 42 AND 47 gpm	[gpm]	43	42	42			
19. WET SCRUBBER WATER PRESSURE MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	[psig]	21	_21	21			
20. WET SCRUBBER AIR PRESSURE AT INLET [POINT B]	["H20"]	_2	2	_2			
21. WET SCRUBBER AIR PRESSURE AT OUTLET [POINT C]	["H20"]	.5	15	5			
22. WET SCRUBBER DIFFERENTIAL PRESSURE	["H20"]	1.5	1.5	1.5			
[POINT B-C] Maintain between 1.0 and 4.5 inches of water							
21. FRESH WATER TO REACTOR	[gpm]	<u> </u>					
22. PETRO TO PRODUCT ON FILTER	[gpm]	3.5	3.5	_3.5			
23. RINSE WATER TO PRODUCT ON FILTER	[gpm]	7.0	7.0	7.0			
PRODUCT SCREEN ANALYSIS		SAMPLE	SAMPLE	SAMPLE			
+60 +100 { Should b	a loss than 201	./6	.05	.5			
	e less than 20] e less than 70]	39 E	54.2	100.1			
•	e less than 30]	36.2	29.6	210.5			
	e less than 10]	19:2	11.8	8.6			
** If you are not able to maintain the above para	-	d contact Gene Trawi					
Condition of Y-Strainer?:		you have to Clean it		nately.			
REMARKS:			-				

DATE: <u> 7/5/11</u>	LOT #:	11-339	SFSOR	PFS PRODUCTION	I (circle one)
A OPERATOR:	HANCEY		SHIFT:	ZNE	
PRODUCT DRYING	START TIME:	<u>1405</u> period that product passes			21:37
	START TIME:	period mat product passes	anough the	STOP TIME:	
	START TIME:			STOP TIME:	
		TIME 1		TIME 2	TIME 3
1. FLOWS ON TIME		1540			
2. FILTER START TIME		1605			
3. FLOWS OFF TIME		2120			
4. SCREWS DOWN TIME		21:37		enalis — augusti di decanisti decanisti dana	
5. TIME		1705		1905	2105
6. BURNER EXIT TEMP		VA		MA	NIA
7. DRYER EXIT TEMP		380	_	372	371
8. VENT FAN AMPS		25		25	25
9. DRAFT FAN AMPS		70		70	70
10. CHLORIDES		69.0		17.0	16.0
DOWN TIMES AND REASON	NS:				
RAW MATERIALS USAGE	EG A				
TANK NUMBER:				<u>KCL</u>	
BEGIN OUTAGE:	4'4'		\leq		
END OUTAGE:	6 6/2"				
USAGE:	24 1/2"				
NUMBER OF LIQUID BRINE TI	RUCKS UNLOADED	¥			
NUMBER OF SALT TRUCKS	S UNLOADED:				
NUMBER OF ACID TRUCKS		_4			
NUMBER OF ACID RAILCA	RS UNLOADED.	ø			

Ø 15:10

1/2 BAG

PETRO USED IN BATCHING

TIME OF BATCHING PETRO

REMARKS:

KC INDUSTRIES, LLC.

i. c

DAILY QUALITY CONTROL AND PRODUCTION LOG 1.11.220

DATE: 12-5-11 LOT #:						
BOPERATOR: Sacht			SHIFT:			
		<u>SAMPLE</u>		SAMPLE		SAMPLE
1. TIME	F4 33	1795		110	-	2105
2. PRODUCTION RATE Start plant at 105 tpd and go to 120- tpd once - 325 < 10%	[tpd]	110-	•		-	
3. ACID [FSA] FLOW	[gpm]	54		_50	-	50
4. ACID [FSA] SPECIFIC GRAVITY		1211		1211	-	1211
5. ACID [FSA] STRENGTH	%	23.75	1	23.75	_	23.75
6. KCL/SALT BRINE FLOW	[gpm]	_50		45.5	-	45.5
7. KCL/SALT BRINE SPECIFIC GRAVITY		1201		1/48	-	1190
8. COLOR OF BRINE		white	,	white	-	inh the
white, yellow, tan, brown] 9. COLOR OF ACID		upla		Yella		urllan
white, yellow, tan, brown]					-	4/
10. REACTOR NO. 1 TEMP [PFS ONLY]	[F]		• *		-	
Maintain between 110 and 140 degrees 11. DRYER TEMPERATURE	[F]	375		270		268
Maintain between 310 and 350 degrees	[1.]				-	
12. VACUUM READING	["Hg]	14			-	
Maintain between 12 and 18	[17]	290		972.		9 <i>80</i> '
13. PRODUCT TEMPERATURE	[F]	100		<u>+12</u> 50	-	10
14. VENTURI SCRUBBER WATER FLOW RATE WAINTAIN BETWEEN 50 AND 55 gpm	[gpm]				-	<u></u>
15. VENTURI SCRUBBER AIR PRESSURE AT IN	LET ["H20"]	10		10	_	10
[POINT A]	JTLET ["H20"]	2	-	2	-	1-
16. VENTURI SCRUBBER AIR PRESSURE AT OU [POINT B]					-	
17. VENTURI SCRUBBER DIFFERENTIAL PRESS	SURE ["H20"]	<u> </u>	•		_	
[POINT A-B] Maintain between 8 and 14 inches of water	[]	¥2		41		42
18. WET SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 42 AND 47 gpm	[gpm]			11-	-	10
19. WET SCRUBBER WATER PRESSURE	[psig]	21		21	-	_21
MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	[11] [0.01]	9		9		2
20. WET SCRUBBER AIR PRESSURE AT INLET [POINT B]	["H20"]	<u> </u>		<u>_</u>	-	
21. WET SCRUBBER AIR PRESSURE AT OUTLE	Т ["H2O"]	.5		.5		.5
[POINT C]			•			
22. WET SCRUBBER DIFFERENTIAL PRESSURE	["H20"]	<u>_/.5</u>		1.5	-	<u> </u>
[POINT B-C] Maintain between 1.0 and 4.5 inches of water	[]					./
21. FRESH WATER TO REACTOR 22. PETRO TO PRODUCT ON FILTER	[gpm]	24.0		¥.0	-	10
,	[gpm]	7.0			-	7.0
23. RINSE WATER TO PRODUCT ON FILTER	[gpm]		206	7.0	2005	
PRODUCT SCREEN ANALYSIS		SAMPLE	1205	SAMPLE		SAMPLE
+60 +100 [S	Should be less than 20]	<u>,05</u> 7.0	,03 7.6	17	2.1	108
· • •	Should be less than 70]	59.6	55.4	51.9	57.6	55.4
-	Should be less than 30]	22.1	26	127.4	27.8	26.2
•	Should be less than 10]	11.5	10.4	11.5	10.9	10.2
** If you are not able to maintain the abo				-	immediatel	у.
Condition of Y-Strainer?: 0/	Did	you have to C	lean it? 💋	10		

REMARKS:

10 - 10 - 10 - 10 - 10 - 10 - 10 - 10 -	KC IND DAILY QUALITY CON	USTRIES, LLC. FROL AND PRODUCT	ION LOG	I)
DATE: <u>17/11/11</u>	LOT #: <u>K11-344</u>	<u>/</u>	FS OR PFS PRODUCTIO	N [circle one]
A OPERATOR: DOB	son)		HIFT: <u>5</u> 7	
PRODUCT DRYING	START TIME: [* defined as the time perio	DISTO d that product passes thro	STOP TIME:	1325
·•	START TIME:	Na ny Tanàna mandritry dia kaominina dia kaominina dia kaominina dia kaominina dia kaominina dia kaominina dia k	STOP TIME:	
	START TIME:	uggalazing nanyang silikati kuka salikati na ba takan manganakati kata	STOP TIME:	and water a substitution of the state of the
		TIME 1	TIME 2	TIME 3
1. FLOWS ON TIME		0/10		
2. FILTER START TIME		0450		
3. FLOWS OFF TIME		1300		A SECTION OF A DESCRIPTION OF A
4. SCREWS DOWN TIME		1325		
5. TIME		0750	0950	1150
6. BURNER EXIT TEMP		NA	W/A	<u>w/w</u>
7. DRYER EXIT TEMP		3420	363'	370
8. VENT FAN AMPS		- 74	24	24
9. DRAFT FAN AMPS		70	70	
10. CHLORIDES		- Zelo	3.1	12.0
DOWN TIMES AND REASONS	3:			
RAW MATERIALS USAGE				a managan dan di sana yang kang kang kang kang kang kang kang k
TANK NUMBER:			KCL	
BEGIN OUTAGE :	61711			1979 - Angling and Saman Sa

		FSA		KCL	
TANK NUMBER:	2	LOIX	nanghada minanga ginili nanga		Freesawayay tool an en travelar outer
BEGIN OUTAGE :	6'7"				
END OUTAGE:	911				
USAGE:	30''				\
NUMBER OF LIQUID BRINE TRU	CKS UNLOADED)			
NUMBER OF SALT TRUCKS U	NLOADED:		0		
NUMBER OF ACID TRUCKS U	NLOADED:		2		
NUMBER OF ACID RAILCARS	UNLOADED:				
NUMBER OF KCL RAILCARS	UNLOADED:		0		
TIME OF BATCHING PETRO			2130 on 12/5/11		
PETRO USED IN BATCHING			1/4		

REMARKS:

date: <u>1,2-1e-11</u> lot #: <u>K11-</u>	340	SFS OR	SFS OR PFS PRODUCTION [circle one]			
BOPERATOR: <u>Sylvia</u>		SHIFT: 154				
·	- <u></u>	SAMPLE	SAMPLE	SAMPLE		
1. TIME		0750	0950	1150		
2. PRODUCTION RATE Start plant at 105 tpd and go to 120- tpd once - 325 < 10%	[tpd]	120	120	<u>_110_</u>		
B. ACID [FSA] FLOW	[gpm]	55.5	55.	52.4		
ACID [FSA] SPECIFIC GRAVITY		lain	1210	1210		
ACID [FSA] STRENGTH	%	Q3. 6%	23.10%	23.10°		
. KC L/SALT BRINE FLOW	[gpm]	49.5	47.4	45.7		
. KC L/SALT BRINE SPECIFIC GRAVITY		1201	1193	1156		
COLOR OF BRINE		CIEAR	CLEAR	CLEAR		
hite, yellow, tan, brown] • COLOR OF ACID		Vellow	Yellow	salles		
hite, yellow, tan, brown]		yenow	JEILDW	- yenou		
0. REACTOR NO. 1 TEMP [PFS ONLY]	[F]	<u> </u>	<u> </u>	_ <u>_</u> X		
laintain between 110 and 140 degrees		2000	20.0	2000		
1. DRYER TEMPERATURE laintain between 310 and 350 degrees	[F]	358	340	382		
2. VACUUM READING	["Hg]	13.5	14.D	14.0		
aintain between 12 and 18	[6]	<u></u>	<u> </u>	······		
3. PRODUCT TEMPERATURE	[F]	216	294	278		
4. VENTURI SCRUBBER WATER FLOW RATE AINTAIN BETWEEN 50 AND 55 gpm	[gpm]	50		50		
5. VENTURI SCRUBBER AIR PRESSURE AT INLET	["H20"]	10	10	_10		
[POINT A] 6. VENTURI SCRUBBER AIR PRESSURE AT OUTLET [POINT B]	["H20"]	3	_2	Z		
7. VENTURI SCRUBBER DIFFERENTIAL PRESSURE	["H20"]	8	8	8		
[POINT A-B] Maintain between 8 and 14 inches of water				······································		
8. WET SCRUBBER WATER FLOW RATE AINTAIN BETWEEN 42 AND 47 gpm	[gpm]	42	_42	42		
9. WET SCRUBBER WATER PRESSURE AINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	[psig]	21	_21	_21		
0. WET SCRUBBER AIR PRESSURE AT INLET [POINT B]	["H20"]	2	_2	_2		
I. WET SCRUBBER AIR PRESSURE AT OUTLET	["H2O"]	.5	.5	.5		
[POINT C] 2. WET SCRUBBER DIFFERENTIAL PRESSURE	["H2O"]	1.5	1.5	1.5		
[POINT B-C] Maintain between 1.0 and 4.5 inches of water	[1120]		_1.5			
I. FRESH WATER TO REACTOR	[gpm]	\times	X	×		
2. PETRO TO PRODUCT ON FILTER	[gpm]	3.5	3.5	3.5		
3. RINSE WATER TO PRODUCT ON FILTER	[gpm]	4.0	4.0	W.0		
RODUCT SCREEN ANALYSIS		SAMPLE	SAMPLE	SAMPLE		
+60		.12	.11	.08		
-	be less than 20]	6.5	6.0	10.2		
-	be less than 70]	48.8	56.3	56.0		
-	be less than 30]	30.0	<u> </u>	24.1		
-	be less than 10]	13.1	9.8	13.3		
** If you are not able to maintain the above parendition of Y-Strainer?:		d contact Gene Trawi you have to Clean it		liately.		

Condition of a Stramol	
REMARKS:	

629		INDUSTRIES, LLC. ONTROL AND PRODUCTIO	NIOC	\mathcal{O}
date: <u>//////</u> a operator: <u>////</u>	LOT #: <u>KII-</u>		R PFS PRODUCTIO	N [circle one]
PRODUCT DRYING	START TIME: [* defined as the time p	<u>1700</u> eriod that product passes through	STOP TIME:	7145
	START TIME:		STOP TIM <u>E:</u>	
	START TIME:		STOP TIM <u>E:</u>	nalogiyaTTCMST44444Mataton aliyasiyasiyasiyasiyasi
		TIME 1	TIME 2	TIME 3
1. FLOWS ON TIME		1600		
2. FILTER START TIME		1700		
3. FLOWS OFF TIME		2130		
4. SCREWS DOWN TIME		2145		
5. TIME	<u></u>	1800	2000	
6. BURNER EXIT TEMP		NA	NA	
7. DRYER EXIT TEMP		374	380	1998 P.M. 1998 P.M. 199
8. VENT FAN AMPS		25	25	
9. DRAFT FAN AMPS		70	70	S. Start South Start Start Start Start Start Start
10. CHLORIDES	•	9.2	11.5	
		l cut d		

DOWN TIMES AND REASONS:	Proplems	with	Fittral) 1) Mim	un alungare	
		-	,		1 8/8	

RAW MATERIALS USAGE

		<u>FSA</u>				<u>KCL</u>		
TANK NUMBER:	3		a Sharahan ya kuta kuta kuta kuta kuta kuta kuta kut		and the second	-	104179838+c5w44-0429578248438444459445	
BEGIN OUTAGE:	3'[["						in tardis ta a tardi an sa fi fi fi fi fi fi fi fa a tarang References dela des partes de fi	
END OUTAGE:	5'8'/2"			at.	المالة الراجعة عن المراجع من المراجع ا المراجع المراجع			
USAGE:	211/2"		elista (wakamin manana a sa			-		
NUMBER OF LIQUID BRINE TRUC	CKS UNLOADE)	Ø					
NUMBER OF SALT TRUCKS U	NLOADED:		Ø					
NUMBER OF ACID TRUCKS UI	NLOADED:		4					
NUMBER OF ACID RAILCARS	UNLOADED:		0					
NUMBER OF KCL RAILCARS	UNLOADED:		Ø					
TIME OF BATCHING PETRO			1/2					
PETRO USED IN BATCHING			1335					

REMARKS:

KC INDUSTRIES, LLC.

DAILY QUALITY CONTROL AND PRODUCTION LOG

B OPERATOR: $(Add C)'' = (Add C)'' = (Add$	DATE: 12-6-11 LOT #:	k11-340	_ SFP	OR PFS F	RODUCT	ION [circl	e onej
I. TIME 1200 90 2. PRODUCTION RATE [tpd] 120 120 3. ACD [FSA] FLOW [gpm] 50 5^{-9} 3. ACD [FSA] SPECIFIC GRAVITY 1231 12333 12333 5. ACD (FSA] STRENGTH 94 $95 \cdot 75$ 144 414	BOPERATOR: Sade-S		S	HIFT:	274		
2. PRODUCTION RATE [prof] $\frac{1}{22}$ $\frac{1}{12}$ $\frac{1}{$							SAMPLE
The part of the angle of Edu Graves 10% [gm] $\frac{50}{2}$ $\frac{59}{2}$ A ACID [FSA] SPECIFIC GRAVITY $\frac{1231}{1233}$ A ACID [FSA] STREINGTH $\frac{50}{25.75}$ $\frac{14}{44}$ A CID [FSA] STREINGTH $\frac{9}{6}$ $\frac{25.75}{144}$ A CID (FSA] STREING FLOW [gm] $\frac{41}{155}$ $\frac{17}{1174}$ $\frac{119}{44}$ A CID (FSA] STREING SPECIFIC GRAVITY $\frac{119}{155}$ $\frac{1174}{119}$ A CID (FSA) STREINE SPECIFIC GRAVITY $\frac{119}{125}$ $\frac{1174}{119}$ A CID (FSA) STREINE SPECIFIC GRAVITY $\frac{119}{119}$ $\frac{1174}{119}$ $\frac{1174}{119}$ $\frac{1174}{119}$ A CID (FSA) STREINE SPECIFIC GRAVITY $\frac{119}{110}$ $\frac{11}{100}$ $\frac{11}{10}$ $\frac{11}{100}$ $\frac{11}{100$	1. TIME		2 4 m		other designment of the local division of th		
3. ACID [FSA] FLOW [gm] $\frac{50}{1221}$ $\frac{52}{1233}$ 4. ACID [FSA] SPECIFIC GRAVITY $\frac{1221}{1233}$ 5. ACID [FSA] STRENGTH 96 $\frac{25}{125}$ $\frac{14}{14}$ 6. KCL/SALT BRINE FLOW [gm] $\frac{175}{145}$ $\frac{1174}{145}$ $\frac{1174}{145}$ 7. KCL/SALT BRINE FLOW [gm] $\frac{1155}{115}$ $\frac{1174}{145}$ $\frac{49}{14}$ 7. KCL/SALT BRINE SPECIFIC GRAVITY $\frac{1155}{115}$ $\frac{1174}{145}$ $\frac{1174}{145}$ $\frac{1174}{145}$ 8. COLOR OF ARTINE SPECIFIC GRAVITY $\frac{1155}{145}$ $\frac{1174}{145}$ $\frac{1174}{14$		[tpd]	120		122	-	8707000-0100-00-0100-00-00
Correction (Correction of the set		[gnm]	50		50		
5. ACID [FSA] STRENGTH % 25.75 44 6. KCL/SALT BRINE FLOW [gpm] $4B$ 7. KCL/SALT BRINE SPECIFIC GRAVITY 8. COLOR OF BRINE SPECIFIC GRAVITY 9. COLOR OF BRINE 9. COLOR OF BRINE 9. COLOR OF CACD 9. COLOR OF ACID 9. COLOR OF ACID ACID ACID 9. COLOR OF ACID ACID 9. COLOR OF ACID ACID 9. COLOR OF ACID ACID 9. COLOR OF ACID ACID ACID 9. COLOR OF ACID ACID ACID	4	[8]]	1231		1233		ويستعودون المتراسية بريسانه بمرد
6. KCL'SALT BRINE FLOW [gpm] $\frac{43}{115}$ $\frac{49}{1179}$ $\frac{49}{1150}$ 7. KCL'SALT BRINE SPECIFIC GRAVITY $\frac{49}{1150}$ $\frac{1179}{1150}$ 11		%	15,75		24		
7. KCL/SALT BRINE SPECIFIC GRAVITY $1/55^{-}$ $1/74^{-}$ $1/65^{-}$ 8. COLOR OF BRINE $4/41^{-}$ $4/41^{-}$ $4/41^{-}$ $4/41^{-}$ 9. COLOR OF ACID $4/41^{-}$ $4/41^{-}$ $4/41^{-}$ $4/41^{-}$ 9. COLOR OF ACID $4/41^{-}$ $4/41^{-}$ $4/41^{-}$ $4/41^{-}$ 9. COLOR OF ACID $4/41^{-}$ $4/41^{-}$ $4/41^{-}$ $4/41^{-}$ 10. REACTOR NO. 1 TEMP [PFS ONLY] [F] $ -$ 11. DRYER TEMPERATURE [F] $2/1^{-}$ $2/16^{-}$ $-$ 11. DRYER TEMPERATURE [F] $2/1^{-}$ $2/16^{-}$ $-$ 12. VACUUM READING ["Hg] $1/4^{-}$ $1/4^{-}$ $-$ Maintain balves on 12 and 16 [F] $2/1^{-}$ $2/8^{-}$ $-$ 13. PRODUCT TEMPERATURE [F] $2/1^{-}$ $2/8^{-}$ $ -$ 14. VENTURI SCRUBBER MATER FLOW RATE [gpm] 5^{-} 4^{-2} $ -$ </td <td></td> <td></td> <td>48</td> <td>•</td> <td>44</td> <td>•</td> <td></td>			48	•	44	•	
8 COLOR OF BRINE $\frac{\sqrt{k+1}}{ $		[OP]	1155 - 10	174 -	1180	L Contraction of the second seco	
9. COLOR OF ACID 9. COLOR OF			shift	·	vhite	•	
points, security in normal problem of the problem			1 nolla	·	. lla		
Maintain between 110 and 140 degrees IF $\frac{273}{27}$ $\frac{273}{27}$ 11. DRYER TEMPERATURE [F] $\frac{273}{27}$ $\frac{273}{27}$ 11. DRYER TEMPERATURE [F] $\frac{273}{27}$ $\frac{273}{27}$ 12. VACUUM READDING ["Hg] $\frac{17}{2}$ $\frac{17}{2}$ 13. PRODUCT TEMPERATURE [F] $\frac{271}{2}$ $\frac{17}{2}$ 14. VENTURI SCRUBBER WATER FLOW RATE [gpm] $\frac{5}{2}$ $\frac{5}{2}$ MAINTAIN BETWEEN 50 AND 65 gpm MAINTAIN SERVEBED 60 AND 65 gpm $\frac{17}{12}$ $\frac{17}{12}$ $\frac{17}{12}$ 15. VENTURI SCRUBBER AIR PRESSURE AT OUTLET ["H20"] $\frac{2}{2}$ $\frac{17}{12}$ $\frac{17}{12}$ 16. VENTURI SCRUBBER MATER FLOW RATE [gpm] $\frac{17}{2}$ $\frac{17}{2$			<u> </u>		491100		
11. DRYER TEMPERATURE [F] $\frac{273}{2}$ $\frac{273}{2}$ Maintain between 30 and 380 degrees ["Hg] $\frac{14}{2}$ $\frac{14}{2}$ Maintain between 12 and 18 [F] $\frac{273}{2}$ $\frac{273}{2}$ 13. PRODUCT TEMPERATURE [F] $\frac{274}{2}$ $\frac{14}{2}$ 14. VENTURI SCRUBBER WATER FLOW RATE [gpm] $\frac{5}{2}$ $\frac{42}{4}$ MAINTAIN BETWEEN 50 AND 56 gpm 15. VENTURI SCRUBBER AIR PRESSURE AT OUTLET ["H20"] $\frac{12}{2}$ $\frac{1}{2}$ 16. VENTURI SCRUBBER DIFFERENTIAL PRESSURE ["H20"] $\frac{2}{3}$ $\frac{3}{2}$ $\frac{1}{2}$ 17. VENTURI SCRUBBER VATER FLOW RATE [gpm] $\frac{\sqrt{2}}{2}$ $\frac{\sqrt{2}}{2}$ $\frac{\sqrt{2}}{2}$ 18. WET SCRUBBER VATER FLOW RATE [gpm] $\frac{\sqrt{2}}{2}$ $\frac{\sqrt{2}}{2}$ $\frac{\sqrt{2}}{2}$ MAINTAIN ETWEEN 20 AND 27 gpm [psig] $\frac{21}{2}$ $\frac{2}{2}$ $\frac{\sqrt{2}}{2}$ 19. WET SCRUBBER WATER FLOW RATE [psig] $\frac{21}{2}$ $\frac{\sqrt{2}}{2}$		[F]					
Maintain between 310 and 360 degrees Image: Constraint of the second secon			275		シッタ・		
12. VACUUM READING ["Hg] $\frac{12}{4}$ $\frac{14}{4}$ Maintain between 12 and 18 [F] $\frac{12}{4}$ $\frac{12}{4}$ $\frac{12}{4}$ 13. PRODUCT TEMPERATURE [F] $\frac{12}{4}$ $\frac{12}{4}$ $\frac{12}{4}$ $\frac{12}{4}$ 14. VENTURI SCRUBBER WATER FLOW RATE [gpm] $\frac{12}{4}$ $\frac{12}{4}$ $\frac{12}{4}$ $\frac{12}{4}$ MAINTAIN BETWEEN 50 AND 55 gpm 15. VENTURI SCRUBBER AIR PRESSURE AT OUTLET ["H20"] $\frac{12}{2}$ $\frac{12}{4}$ $\frac{12}{4}$ POINT A POINT A POINT A $\frac{12}{900 \text{ Maintain between 8 and 14 inches of water \frac{12}{8} \frac{12}{8} \frac{12}{8} \frac{12}{8} \frac{12}{8} \frac{12}{8} \frac{12}{8} \frac{12}{8} \frac{12}{8} \frac{12}{10} $		[F]	3/3		310		N-12010101010101010101010101010
Maintain between 12 and 18 [F] $\frac{270}{12}$ $\frac{288}{2}$ 13. PRODUCT TEMPERATURE [F] $\frac{270}{12}$ $\frac{288}{2}$ 14. VENTURI SCRUBBER WATER FLOW RATE [gpm] $\frac{5^{\circ}}{2}$ $\frac{4^{\circ}}{2}$ 15. VENTURI SCRUBBER AIR PRESSURE AT INLET ["H20"] $\frac{10}{12}$ $\frac{10}{12}$ 16. VENTURI SCRUBBER DIFFERENTIAL PRESSURE ["H20"] $\frac{2}{2}$ $\frac{10}{2}$ 17. VENTURI SCRUBBER DIFFERENTIAL PRESSURE ["H20"] $\frac{2}{3}$ $\frac{10}{12}$ 17. VENTURI SCRUBBER MATER FLOW RATE [gpm] $\frac{\sqrt{2}}{2}$ $\frac{\sqrt{2}}{2}$ 18. WET SCRUBBER WATER FLOW RATE [gpm] $\frac{\sqrt{2}}{2}$ $\frac{\sqrt{2}}{2}$ 19. WET SCRUBBER AIR PRESSURE [psig] $\frac{21}{2}$ $\frac{2}{2}$ 10. WET SCRUBBER AIR PRESSURE AT INLET ["H20"] $\frac{5}{5}$ $\frac{7}{5}$ 10. WET SCRUBBER AIR PRESSURE AT OUTLET ["H20"] $\frac{5}{5}$ $\frac{7}{5}$ 10. WET SCRUBBER DIFFERENTIAL PRESSURE [m20"] $\frac{1}{5}$ $\frac{7}{5}$ 20. WET SCRUBBER AIR PRESSURE AT OUTLET ["H20"] $\frac{5}{5}$ $\frac{7}{5}$ 12. WET SCRUBBER DIFFERENTIAL PRESSURE [m20"] $\frac{1}{5}$ $\frac{7}{5}$	-	["Hg]	14		14		
14. VENTURI SCRUBBER WATER FLOW RATE [gpm] 5° 5° 5° MAINTAN BETWEEN 50 AND 55 gpm 15. VENTURI SCRUBBER AIR PRESSURE AT NLET ["H20"] 10° 10° 10° 15. VENTURI SCRUBBER AIR PRESSURE AT OUTLET ["H20"] 2° 10° 10° 10° 16. VENTURI SCRUBBER AIR PRESSURE AT OUTLET ["H20"] 2° 10° 10° 10° 17. VENTURI SCRUBBER MATER PRESSURE ["H20"] 2° 10° 10° 10° 18. WET SCRUBBER WATER FLOW RATE [gpm] 10° 10° 10° 10° 10° 19. WET SCRUBBER WATER PRESSURE [psig] 21° 2° <		101	171	•	002'		
MAINTAIN BETWEEN 50 AND 55 gpm 15. VENTURI SCRUBBER AIR PRESSURE AT INLET ["H20"] $\frac{1}{2}$ $\frac{1}{2}$ [POINT A] 16. VENTURI SCRUBBER AIR PRESSURE AT OUTLET ["H20"] $\frac{2}{3}$ $\frac{3}{6}$ [POINT AB] Maintain between 8 and 14 inches of water [POINT AB] Maintain between 8 and 14 inches of water 18. WET SCRUBBER WATER FLOW RATE [gpm] $\frac{1}{2}$ $\frac{1}{2}$ $\frac{1}{2}$ 19. WET SCRUBBER WATER PRESSURE [Psig] $\frac{2}{2}$ $\frac{1}{2}$ $\frac{1}{2}$ $\frac{1}{2}$ MAINTAIN BETWEEN 42 AND 70 gpm 19. WET SCRUBBER AIR PRESSURE [Psig] $\frac{2}{2}$ $\frac{1}{2}$ $\frac{1}{2}$ $\frac{1}{2}$ MAINTAIN BETWEEN 42 AND 70 gpm 19. WET SCRUBBER AIR PRESSURE [Psig] $\frac{2}{2}$ $\frac{1}{5}$ $\frac{1}{5}$ 10. WET SCRUBBER AIR PRESSURE AT INLET ["H20"] $\frac{5}{5}$ $\frac{5}{5}$ [POINT C] 21. WET SCRUBBER AIR PRESSURE AT OUTLET ["H20"] $\frac{5}{5}$ $\frac{1}{5}$ $\frac{5}{5}$ [POINT C] 22. WET SCRUBBER DIFFERENTIAL PRESSURE ["H20"] $\frac{1}{5}$ $\frac{1}{5}$ $\frac{5}{5}$ [POINT C] 23. RINSE WATER TO REACTOR [gpm] $\frac{2}{2}$ $\frac{2}{7}$ $\frac{1}{2}$ $\frac{1}{2}$ $\frac{2}{7}$ +60 +100 [Should be less than 20] $\frac{4}{5}$ $\frac{2}{5}$ $\frac{7}{7}$ $\frac{3}{3}$ $\frac{3}{5}$ +60 +100 [Should be less than 30] $\frac{2}{3}$ $\frac{2}{5}$ $\frac{7}{5}$ $\frac{3}{3}$ $\frac{3}{5}$ $\frac{7}{5}$ $\frac{3}{3}$ $\frac{3}{5}$ $\frac{1}{5}$ $\frac{1}{$	13. PRODUCT TEMPERATURE	[F]	210		198_		
15. VENTURI SCRUBBER AIR PRESSURE AT INLET ["H20"] $\frac{10}{2}$ $\frac{10}{2}$ 16. VENTURI SCRUBBER AIR PRESSURE AT OUTLET ["H20"] $\frac{2}{2}$ $\frac{1}{2}$ [POINT 8] 10. VENTURI SCRUBBER DIFFERENTIAL PRESSURE ["H20"] $\frac{2}{2}$ $\frac{1}{2}$ [POINT 8] Inches of water [gpm] $\frac{1}{2}$ $\frac{1}{2}$ $\frac{1}{2}$ 18. WET SCRUBBER WATER FLOW RATE [gpm] $\frac{1}{2}$ $\frac{1}{2}$ $\frac{1}{2}$ 19. WET SCRUBBER WATER FRESSURE [psig] $\frac{2}{1}$ $\frac{2}{2}$ $\frac{1}{2}$ 19. WET SCRUBBER AIR PRESSURE [psig] $\frac{2}{1}$ $\frac{2}{2}$ $\frac{2}{2}$ 20. WET SCRUBBER AIR PRESSURE AT OUTLET ["H20"] $\frac{5}{5}$ $\frac{7}{5}$ $\frac{7}{5}$ 10. WET SCRUBBER AIR PRESSURE AT OUTLET ["H20"] $\frac{5}{5}$ $\frac{7}{5}$ $$		E [gpm]	50		<u> </u>	•	
IPOINT AJ16. VENTURI SCRUBBER AIR PRESSURE AT OUTLET["H20"] 2 2 IPOINT BJ17. VENTURI SCRUBBER DIFFERENTIAL PRESSURE["H20"] 3 8 17. VENTURI SCRUBBER DIFFERENTIAL PRESSURE["H20"] 3 8 18. WET SCRUBBER WATER FLOW RATE[gpm] $4/2$ $4/2$ MAINTAIN BETWEEN 42 AND 47 gpm19. WET SCRUBBER WATER PRESSURE[psig] 21 19. WET SCRUBBER AIR PRESSURE AT INLET["H20"] 2 2 20. WET SCRUBBER AIR PRESSURE AT OUTLET["H20"] 5 75 IPOINT BJ21. 21 21 21 21. WET SCRUBBER AIR PRESSURE AT OUTLET["H20"] 5 75 IPOINT B-C] Maintain between 1.0 and 4.5 inches of water 1.5 1.5 1.5 22. PETRO TO PRODUCT ON FILTER[gpm] 2.9 7.0 7.0 23. RINSE WATER TO PRODUCT ON FILTER[gpm] 7.0 7.0 7.0 PRODUCT SCREEN ANALYSISSAMPLE 5.47 7.9 7.0 +100[Should be less than 20] 7.0 7.0 7.0 +220[Should be less than 30] 7.0 7.0 7.0 +325[Should be less than 30] 7.0 7.0 7.0 +325[Should be less than 30] 7.0 7.0 7.0 +400[Should be less than 30] 7.0 7.0 7.0 +525[Should be less than 30] 7.0 7.0 7.0 +525[Should be less than 30] 7.0 7.0 7.0		NI.FT ["H20"]	10		10		
[POINT B]17. VENTURI SCRUBBER DIFFERENTIAL PRESSURE["H20"] $\frac{9}{2}$ $\frac{9}{2}$ [POINT AB] Maintain between 8 and 14 inches of water[gpm] $\frac{1}{\sqrt{2}}$ $\frac{1}{\sqrt{2}}$ $\frac{1}{\sqrt{2}}$ 18. WET SCRUBBER WATER FLOW RATE[gpm] $\frac{1}{\sqrt{2}}$ $\frac{1}{\sqrt{2}}$ $\frac{1}{\sqrt{2}}$ 19. WET SCRUBBER WATER PRESSURE[psig] 21 21 21 19. WET SCRUBBER AIR PRESSURE AT INLET["H20"] 2 2 20. WET SCRUBBER AIR PRESSURE AT OUTLET["H20"] 5 65 [POINT 6]21. WET SCRUBBER AIR PRESSURE AT OUTLET["H20"] 5 65 21. WET SCRUBBER DIFFERENTIAL PRESSURE["H20"] 1.5 1.5 7.6 22. WET SCRUBBER DIFFERENTIAL PRESSURE["H20"] 1.5 1.5 7.6 23. RINSE WATER TO REACTOR[gpm] 2.9 7.0 7.0 23. RINSE WATER TO PRODUCT ON FILTER[gpm] 7.0 7.0 PRODUCT SCREEN ANALYSIS $8AMPLE$ $8AMPLE$ $8AMPLE$ +60 7.5 7.6 7.6 +100[Should be less than 20] 7.5 7.5 +220[Should be less than 30] 7.5 7.5 +325[Should be less than 30] 7.5 7.5 ** If you are not able to maintain the above parameters, you should contact Gene Travick or Dean Qualls immediately.Condition of Y-Strainer?: $0 \neq$ Did you have to Clean it? $f/0$				•	<u></u>	•	
17. VENTURI SCRUBBER DIFFERENTIAL PRESSURE ["H20"] $\frac{7}{2}$ $\frac{9}{1/2}$ [POINT A-B] Maintain between 8 and 14 inches of water [gpm] $\frac{1}{2}$ $\frac{1}{2}$ 18. WET SCRUBBER WATER FLOW RATE [gpm] $\frac{1}{2}$ $\frac{1}{2}$ 19. WET SCRUBBER WATER PRESSURE [psig] 21 21 20. WET SCRUBBER AIR PRESSURE AT INLET ["H20"] 2 2 19. WET SCRUBBER AIR PRESSURE AT OUTLET ["H20"] $.5$ $.65$ 21. WET SCRUBBER AIR PRESSURE AT OUTLET ["H20"] $.5$ $.65$ 21. WET SCRUBBER DIFFERENTIAL PRESSURE ["H20"] $.5$ $.65$ 22. WET SCRUBBER DIFFERENTIAL PRESSURE ["H20"] $.5$ $.65$ [POINT G] $$		OUTLET ["H20"]	<u> </u>		<u> </u>	,	
[POINT A-B] Maintain between 8 and 14 inches of water18. WET SCRUBBER WATER FLOW RATE[gpm] $\sqrt{2}$ $\sqrt{2}$ 19. WET SCRUBBER WATER PRESSURE[psig] 21 2.1 20. WET SCRUBBER AIR PRESSURE AT INLET["H20"] 2 2 20. WET SCRUBBER AIR PRESSURE AT OUTLET["H20"] 5 65 19. WET SCRUBBER AIR PRESSURE AT OUTLET["H20"] $.5$ $.65$ 21. WET SCRUBBER DIFFERENTIAL PRESSURE["H20"] $.5$ $.65$ 22. WET SCRUBBER DIFFERENTIAL PRESSURE["H20"] $.1.5$ 1.5 21. FRESH WATER TO REACTOR[gpm] 2 2 22. WET SCRUBBER DIFFERENTIAL PRESSURE["H20"] $.1.5$ 1.5 23. RINSE WATER TO REACTOR[gpm] 2 2 PRODUCT SCREEN ANALYSISSAMPLESAMPLESAMPLE $+60$ $.100$ [Should be less than 20] $.52$ $.7.9$ $+200$ [Should be less than 20] $.7.9$ $.7.9$ -325 [Should be less than 30] $.1.5$ $.1.5$ $*$ If you are not able to maintain the above parameters, you should contact Gene Trawick or Dean Quallis immediately.Condition of Y-Strainer?: $0/c$ Did you have to Clean it? $/10$		SSURE ["H20"]	8		8		
MAINTAIN BETWEEN 42 AND 47 gpmImage: constraint of the sprax nozzle[psig] 21 21 21 19. WET SCRUBBER WATER PRESSURE AT INLET[psig] 2 2 20. WET SCRUBBER AIR PRESSURE AT INLET["H20"] $.5$ $.6$ 10. WET SCRUBBER AIR PRESSURE AT OUTLET["H20"] $.5$ $.6$ 21. WET SCRUBBER DIFFERENTIAL PRESSURE["H20"] $.5$ $.6$ 22. WET SCRUBBER DIFFERENTIAL PRESSURE["H20"] $.5$ $.6$ 22. WET SCRUBBER DIFFERENTIAL PRESSURE["H20"] $.5$ $.6$ 21. FRESH WATER TO REACTOR[gpm] $.6$ $.7$ 22. PETRO TO PRODUCT ON FILTER[gpm] $.6$ $.7$ 23. RINSE WATER TO PRODUCT ON FILTER[gpm] $.6$ $.7$ $+60$ [Should be less than 20] $.7$ $.7$ $+200$ [Should be less than 20] $.7$ $.7$ $+325$ [Should be less than 30] $.7$ $.7$ -325 [Should be less than 30] $.7$ $.7$ $**$ If you are not able to maintain the above parameters, you should contact Gene Trawick or Dean Qualls immediately.Condition of Y-Strainer?: $.2$ Did you have to Clean it? $/1.0$.10		sin		
19. WET SCRUBBER WATER PRESSURE[psig] 21 21 MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE 2 20. WET SCRUBBER AIR PRESSURE AT INLET["H20"]POINT B 3 21. WET SCRUBBER AIR PRESSURE AT OUTLET["H20"]POINT C 5 22. WET SCRUBBER DIFFERENTIAL PRESSURE["H20"]POINT C 1.5 21. FRESH WATER TO REACTOR[gpm]22. PETRO TO PRODUCT ON FILTER[gpm]23. RINSE WATER TO PRODUCT ON FILTER[gpm] 460 7.0 $+60$ 7.0 $+60$ 58.47 $+225$ [Should be less than 20] $+325$ [Should be less than 30] -325 [Should be less than 30] -325 [Should be less than 10] $+100$ or $10 ext{ schuld be less than 10]+100 for 10 ext{ schuld be less than 20]-325[Should be less than 10]-325[Should be less than 10]-325[Should be less than 10]-325[Should be less than 10]-12 cdot 11.5-15 cdot 12.5-15 cdot 12.5-16 cdot 12.5-16 cdot 12.5-16 cdot 12.5-17 cdot 12.5-17 cdot 12.5-17 cdot 12.5-$		[gpm]	<u>Y'L</u>		12	,	
MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE 20. WET SCRUBBER AIR PRESSURE AT INLET ["H20"] 2 2 [POINT B] 21. WET SCRUBBER AIR PRESSURE AT OUTLET ["H20"] $.5$ $.5$ $.5$ [POINT C] 22. WET SCRUBBER DIFFERENTIAL PRESSURE ["H20"] 1.5 1.5 $.5$ $.5$ [POINT B-C] Maintain between 1.0 and 4.5 inches of water 21. FRESH WATER TO REACTOR [gpm] 2.9 $.7.9$ 22. PETRO TO PRODUCT ON FILTER [gpm] 2.9 $.7.9$ $.7.9$ 23. RINSE WATER TO PRODUCT ON FILTER [gpm] 2.9 $.7.9$ $.7.9$ PRODUCT SCREEN ANALYSIS SAMPLE SAMPLE $.460$ $.7.9$ $.7$		[psig]	21		21		
20. WET SCRUBBER AIR PRESSURE AT NULLIT[H20]				•	2	•	
21. WET SCRUBBER AIR PRESSURE AT OUTLET ["H20"] .5 .6 [POINT C]		["H20"]	<u> </u>				
[POINT C]Image: Condition of Y-Strainer?:Image: Condition of Y-Strainer?:Im		ET ["Uo0"]	.5		5		
22. WET SCRUBBER DIFFERENTIAL PRESSURE [POINT B-C] Maintain between 1.0 and 4.5 inches of water ["H20"] 1.5 1.5 1.5 21. FRESH WATER TO REACTOR [gpm] 2.9		EI [H20]					
21. FRESH WATER TO REACTOR [gpm] Image: style="text-align: center;">Image: style="text-align: center;">Image: style="text-align: style="text-align: center;">Image: style="text-align: style="text-alig	22. WET SCRUBBER DIFFERENTIAL PRESSUR	E ["H20"]	1.5		15		
22. PETRO TO PRODUCT ON FILTER[gpm] $\frac{14.9}{2.0}$ $\frac{14.9}{7.0}$ 23. RINSE WATER TO PRODUCT ON FILTER[gpm] 2.0 7.0 PRODUCT SCREEN ANALYSISSAMPLESAMPLE+60 47.2 $1/5$ +100[Should be less than 20] 9.5 9.5 9.7 10.7 +200[Should be less than 70] 53.9 53.9 52.7 54.7 54.7 54.7 54.7 53.9 52.7 54.7 53.9 52.7 54.7 53.9 20.47 90.47 1325 [Should be less than 30] 12.6 11.5 10.67 12.78 ** If you are not able to maintain the above parameters, you should contact Gene Trawick or Dean Qualls immediately.Condition of Y-Strainer?: $9/2$ Did you have to Clean it? $f/0$					/		
23. RINSE WATER TO PRODUCT ON FILTER[gpm] $\overline{7.0}$ $\overline{7.0}$ PRODUCT SCREEN ANALYSISSAMPLESAMPLESAMPLE+60							
PRODUCT SCREEN ANALYSISSAMPLESAMPLE+60 27 $e/0$ $1/2$ $1/5$ +100[Should be less than 20] 9.5 4.7 10.47 +200[Should be less than 70] 58.9 57.7 58.7 +325[Should be less than 30] 18.8 20.47 90.47 -325[Should be less than 10] 12.6 11.5 10.67 ** If you are not able to maintain the above parameters, you should contact Gene Trawick or Dean Qualls immediately.Condition of Y-Strainer?: $9/t$ Did you have to Clean it? $1/0$			28				
PRODUCT SCREEN ANALYSIS SAMPLE SAMPLE SAMPLE SAMPLE SAMPLE +60 -40 [Should be less than 20] -27 1/2 1/5 +100 [Should be less than 20] -2.5 -2.7 58.7 54.5 +325 [Should be less than 30] -32.5 [Should be less than 10] -12.6 11.5 10.0 12.6 ** If you are not able to maintain the above parameters, you should contact Gene Trawick or Dean Qualls immediately. Did you have to Clean it? // \wp Did you have to Clean it? // \wp	23. RINSE WATER TO PRODUCT ON FILTER	[gpm]	<u> </u>	1900 .	1.0		-
+100[Should be less than 20] 9.5 $9_{\pm}7$ 10.4 +200[Should be less than 70] 58.9 57.7 58.7 58.7 +325[Should be less than 30] 18.8 $2o.4$ $2o.4$ 90.4 -325[Should be less than 10] 12.6 11.5 10.0 12.8 ** If you are not able to maintain the above parameters, you should contact Gene Trawick or Dean Qualls immediately.Condition of Y-Strainer?: $9/t$			SAMPLE				SAMPLE
+200 [Should be less than 70] 58.9 57.7 58.7 54.5 +325 [Should be less than 30] [B.B 20.4 20.4 20.4 -325 [Should be less than 10] [2.6 11.5 10.0 12.8 ** If you are not able to maintain the above parameters, you should contact Gene Trawick or Dean Qualls immediately. Did you have to Clean it? // Φ				,/0			
+325 [Should be less than 30] 18.8 20.4 20.4 90.4 -325 [Should be less than 10] 12.6 11.5 10.0 12.8 ** If you are not able to maintain the above parameters, you should contact Gene Trawick or Dean Qualls immediately. Did you have to Clean it? // Φ				1:			
-325 [Should be less than 10] ** If you are not able to maintain the above parameters, you should contact Gene Trawick or Dean Qualls immediately. Condition of Y-Strainer?: $\mathcal{O}_{\mathcal{K}}$ Did you have to Clean it? $// \mathcal{O}$		-		tali al anno 1			
** If you are not able to maintain the above parameters, you should contact Gene Trawick or Dean Qualls immediately. Condition of Y-Strainer?: 2/2 Did you have to Clean it? // \$\varnothing\$	-		a second seco				+
Condition of Y-Strainer?: 2/t Did you have to Clean it? // D			واجعا بيرابدها سواحداد تبطيه المتبير ومعالمه المتراجع	awick or I	for a second		<u> </u>
						miniculately	
	a de la constante de			, , , , , , , , , , , , , , , , , , ,			

a start		INDUSTRIES, LLC. ONTROL AND PROD	UCTION LOG	
DATE: <u>17/11/</u>	LOT #: K11-3	941	SFS OR PFS PRODUC	FION [circle one]
A OPERATOR: DOBS	m)		SHIFT:	
PRODUCT DRYING	START TIME: [* defined as the time po	0835 eriod that product passes	STOP TIME through the drying column]	
	START TIME:		STOP TIME	2:
	START TIME:	1903-00-00-00-00-00-00-00-00-00-00-00-00-0	STOP TIME	2:
		TIME 1	TIME 2	TIME 3
1. FLOWS ON TIME		0807) 	
2. FILTER START TIME		083	5	
3. FLOWS OFF TIME		1500		
4. SCREWS DOWN TIME		1515		
5. TIME		0935	1135	1335
6. BURNER EXIT TEMP		NA	NIA	wln
7. DRYER EXIT TEMP		344	374'	348°
8. VENT FAN AMPS		74	24	24
9. DRAFT FAN AMPS		70		70
10. CHLORIDES		18.0	1B. D	14.0
DOWN TIMES AND REASONS:			£	
RAW MATERIALS USAGE				na ya da kana ka
TANK NUMBER:	_ <u></u>	Mandala (ng mga mga Katalan Sala na	<u>KCL</u> .	and The Party of Control of Contr
BEGIN OUTAGE:	5'812"			na ga anna an ann an an ann an ann an ann an a
END OUTAGE:	7'11"	anaranan da yang pertakan da yang mengenten da yang mengenten da yang mengenten da yang mengenten da yang menge		
USAGE:	2612"			
NUMBER OF LIQUID BRINE TRUC NUMBER OF SALT TRUCKS UN NUMBER OF ACID TRUCKS UN NUMBER OF ACID RAILCARS NUMBER OF KCL RAILCARS TIME OF BATCHING PETRO PETRO USED IN BATCHING	NLOADED: NLOADED: UNLOADED:	0 4 0 0 815 1/2		

REMARKS:

1

DATE: [2-7-1] LOT #;	SFS OR PFS PRODUCTION [circle one]				
BOPERATOR: SYLVIA SA		FT: 15t / 3			
		SAMPLE	SAMPLE	SAMPLE	
1. TIME		0935	113.5	1335	
2. PRODUCTION RATE	[tpd]	120	110	110	
Start plant at 105 tpd and go to 120- tpd once - 325 < 10% 3. ACID [FSA] FLOW	[gpm]	49,1	455	43.5	
4. ACID [FSA] SPECIFIC GRAVITY		1234	1234	1234	
5. ACID [FSA] STRENGTH	%	26.196	26.190	26.190	
6. KCL /SALT BRINE FLOW	[gpm]	49.0	45.0	43.5	
7. KCL/ SALT BRINE SPECIFIC GRAVITY		1198	1191	1191	
8. COLOR OF BRINE		CLEAR	CLEAR	CLEAR	
[white, yellow, tan, brown]		·····			
9. COLOR OF ACID [white, yellow, tan, brown]		yellow	Yellow	Yellow	
10. REACTOR NO. 1 TEMP [PFS ONLY]	[F]	<u> </u>	<u> </u>	$\underline{\times}$	
Maintain between 110 and 140 degrees		RIDD	7/1	a to a	
11. DRYER TEMPERATURE	[F]	368	511	348	
Maintain between 310 and 350 degrees 12. VACUUM READING	["Hg]	12.5	12.5	12.5	
Maintain between 12 and 18	[118]	<u>1a.</u>	<u>_/a</u>	$\frac{1}{2}$	
13. PRODUCT TEMPERATURE	[F]	251	281	300	
14. VENTURI SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 50 AND 55 gpm	[gpm]	50	.50	<u>.50</u>	
15. VENTURI SCRUBBER AIR PRESSURE AT IN [POINT A]	ilet ["H20"]	10	10	[b	
16. VENTURI SCRUBBER AIR PRESSURE AT OU [POINT B]	UTLET ["H20"]		2	2	
17. VENTURI SCRUBBER DIFFERENTIAL PRES	SURE ["H20"]	8		8	
[POINT A-B] Maintain between 8 and 14 inches of water 18. WET SCRUBBER WATER FLOW RATE	[gpm]	りは	42	42	
MAINTAIN BETWEEN 42 AND 47 gpm					
19. WET SCRUBBER WATER PRESSURE MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	[psig]	_2	_21	21	
20. WET SCRUBBER AIR PRESSURE AT INLET [POINT B]	["H20"]		_3	<u>a</u>	
21. WET SCRUBBER AIR PRESSURE AT OUTLE [POINT C]	CT ["H20"]	.5	<u>.5</u>	.5	
22. WET SCRUBBER DIFFERENTIAL PRESSURI	E ["H20"]	1.5	1.5	1.5	
[POINT B-C] Maintain between 1.0 and 4.5 inches of water	- []				
21. FRESH WATER TO REACTOR	[gpm]	\times	X	$\mathbf{\dot{x}}$	
22. PETRO TO PRODUCT ON FILTER	[gpm]	3.5	3.5	3.5	
23. RINSE WATER TO PRODUCT ON FILTER	[gpm]	5.0	5.0	5.0	
PRODUCT SCREEN ANALYSIS		SAMPLE	SAMPLE	SAMPLE	
+60		,210 .2		1.25	
•	Should be less than 20]	9.1 11.	7 8,5	/ 11.4	
-	Should be less than 70]		.8 50.6	59.5	
	Should be less than 30]	23.8 20		19.7	
-	Should be less than 10]	23.3 11.	2 16.11	8.4	
** If you are not able to maintain the ab				ately.	
Condition of Y-Strainer?:	Did	you have to Clean i	t?		

REMARKS:

kn ⊶e	DAILY QUAL	KC INDUSTRII		UCTION LO)G	
DATE: <u>12-7-11</u>	lot #: <u>Ki</u>	1-341		SES OR P	FS PRODUCTIO	N [circle one]
A OPERATOR: CHAN	seep			SHIFT:	200	
PRODUCT DRYING) START TIME: [* defined as the	<u>172</u> time period that pr		through the	STOP TIME: drying column]	2143
	START TIME:		nijuch kang ang kang kang kang kang kang kang		STOP TIME:	n for sufficient of the suffic
	START TIME:		ugu alka menyekti kala kushta kushta di kata ta	er dia	STOP TIME:	an séring an sa sing ang séring ang séring ang séring ang séring séring séring séring séring séring séring séri
			TIME 1	1	TIME 2	TIME 3
1. FLOWS ON TIME			1655	_	1010-1010-1010-1010-1010-1010-1010-101	wites a fait is a constant fait by a state of any start of the second
2. FILTER START TIME			1720	ca#1	4564/75940-462574/8933401204745(5)4987475455498749	Energie Street And State Stat
3. FLOWS OFF TIME			2130		1.221, 16.341 (16.221).3740/11 1001 27 67 10 1001 - 4661 1002 1004	W STATES A MIN FILM FILM FOR STATES TO AND THE STATES
4. SCREWS DOWN TIME			2143	قتر <u>ن</u>	wachilik olasaki falamenyena parake deng	Kistorikansi da yasar kontarati akara ya
5. TIME			1820		2020	۲
6. BURNER EXIT TEMP			NIA	عد <u>م</u>	NIA	an a substitution of the
7. DRYER EXIT TEMP			378	aguar an	371	189 (1777) 179 (1777) 199 (1777) 179 (1777) 199 (1777) 179 (1777) 199 (1777) 179 (1777) 179 (1777)
8. VENT FAN AMPS			_26		25	Simily Coxy have been adverted and a second
9. DRAFT FAN AMPS			70		70	PALINGGAMMA WARDONAADAMAADAMAADAMAADAMAADAMA
10. CHLORIDES			22		21	An and the international cost of the state o
DOWN TIMES AND REASONS:		*****	18 29 19 19 20 19 19 19 19 19 19 19 19 19 19 19 19 19			
RAW MATERIALS USAGE	naar baalanaan kan maas maan maan kan kan kan kan kan kan kan kan kan	**************************************	an dh'an an dharan ta channa dhanna dhann	n na	መንስረብ የደለቀበም እና እር እና	and Mit Constant of the Constant o
TANK NUMBER:	3	<u>FSA</u>		The type of the State of the St	KCL	nauti an cen atomo man
BEGIN OUTAGE:	7"(1"			Many Land Constrainty of Constrainty of Constrainty of Constrainty of Constrainty of Constrainty of Constrainty	-	
END OUTAGE:	9'5'		niry,			nan managan ang kang kang kang kang kang kang
USAGE:	18 ''		NG73.		Allera and an and a second and a	K, F. B.C. P. J. Hage Will Strategy with an
NUMBER OF LIQUID BRINE TRUG	CKS UNLOADED	1			•	
NUMBER OF SALT TRUCKS U	NLOADED:	Ŀ	24 (3)			
NUMBER OF ACID TRUCKS U	NLOADED:	<u> </u>				
NUMBER OF ACID RAILCARS		Ø	****			
NUMBER OF KCL RAILCARS	UNLOADED:	Ð				
TIME OF BATCHING PETRO		1515	R.17/3			
PETRO USED IN BATCHING		- 1/.) BAL	2			

REMARKS:

DATE: $\frac{12.7.11}{1.000}$ LOT #: $\frac{12.1.11}{1.000}$	341	OR PFS PRODUCTION [circle one]				
OPERATOR:	ay, manyati wang Tim, Kupingkang Shipata It		T: SAMPLE	SAMPLE		
. TIME		1820	2020	GARINE MA		
PRODUCTION RATE	[tpd]	120	12			
art plant at 105 tpd and go to 120- tpd once - 325 < 10%		119	1/9			
ACID [FSA] FLOW	[gpm]	70	70			
ACID [FSA] SPECIFIC GRAVITY		1235	/235	Kalinayikin ingerikating Dage		
ACID [FSA] STRENGTH	%	26.25	16.23	ar with the strategy with the strategy of the st		
KCL/SALT BRINE FLOW	[gpm]	50	4			
KCL/SALT BRINE SPECIFIC GRAVITY		1196 - 114	1 - 1175	Comments Comments		
COLOR OF BRINE		white	white_			
nite, yellow, tan, brown] COLOR OF ACID		uella-	yella			
nite, yellow, tan, brown]		_ <u></u>				
D. REACTOR NO. 1 TEMP [PFS ONLY]	[F]	Sales and Barrier and Sales and Sales and Sales				
aintain between 110 and 140 degrees		225	278			
1. DRYER TEMPERATURE	[F])/3	310			
aintain between 310 and 350 degrees 2. VACUUM READING	["Hg]	14	14			
aintain between 12 and 18	[118]					
8. PRODUCT TEMPERATURE	[F]	285	277			
4. VENTURI SCRUBBER WATER FLOW RATE	[gpm]	50	50			
AINTAIN BETWEEN 50 AND 55 gpm			an a suite a suite anna an a			
5. VENTURI SCRUBBER AIR PRESSURE AT INLET	["H20"]	10	10			
[POINT A]	(III JoOH	2	2			
6. VENTURI SCRUBBER AIR PRESSURE AT OUTLET [POINT B]	["H20"]		<u> </u>	and a first of the particular state of the s		
7. VENTURI SCRUBBER DIFFERENTIAL PRESSURE	["H20"]	8	ð			
[POINT A-B] Maintain between 8 and 14 inches of water		5 x /2	ci a	Withing Clining and Approximation		
8. WET SCRUBBER WATER FLOW RATE	[gpm]	42	92	······		
AINTAIN BETWEEN 42 AND 47 gpm D. WET SCRUBBER WATER PRESSURE	[psig]	21	21			
NINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	[harg]					
). WET SCRUBBER AIR PRESSURE AT INLET	["H20"]	2	2			
[POINT B]						
I. WET SCRUBBER AIR PRESSURE AT OUTLET	["H20"]	<u>.,5</u>	<u>_</u>			
		15	1.5			
2. WET SCRUBBER DIFFERENTIAL PRESSURE [POINT B-C] Maintain between 1.0 and 4.5 inches of water	["H2O"]		1.2			
I. FRESH WATER TO REACTOR	[gpm]	and the second	Marrie .			
2. PETRO TO PRODUCT ON FILTER	[gpm]	4.0	4.0			
3. RINSE WATER TO PRODUCT ON FILTER		7.0	7.0			
	[gpm]	.1.20				
RODUCT SCREEN ANALYSIS		SPAINER LIN	SPAIVER LIC	SAMPLE		
+60	1 1 m 1 m 001	.27 .13	Characterization of the statement to state a state of the			
	be less than 20] be less than 70]	12.2 9.2	Sine and the second			
	be less than 30]	21.6 27.				
•	be less than 10]	10.6 12.5				
** If you are not able to maintain the above para	-			and a second		

REMARKS:

		INDUSTRIES, LLC. ONTROL AND PRODU	JCTION LOG		Ø
	LOT #: <u> -</u>	342	SFS OR PFS F	RODUCTION	[circle one]
A OPERATOR: DOBS	san		SHIFT:	<u>بح</u> ر	
PRODUCT DRYING	START TIME: [* defined as the time p	eriod that product passes		OP TIME:	1326
	START TIME:			OP TIME:	
	START TIME:	National Science State Science State Science Science Science Science Science Science Science Science Science Sci	ST	OP TIME:	ana ang manakana kana ang mang mang kana ang mang mang mang mang mang mang ma
 FLOWS ON TIME FILTER START TIME FLOWS OFF TIME SCREWS DOWN TIME 		TIME 1 0420 0443 1310 1320		ME 2	TIME 3
5. TIME 6. BURNER EXIT TEMP 7. DRYER EXIT TEMP 8. VENT FAN AMPS 9. DRAFT FAN AMPS 10. CHLORIDES DOWN TIMES AND REASONS:		074 NNA 370 Z4 70 21		<u>0945</u> <u>N/A</u> 3.51° 24 70 19	1145 N/M 367* 27 70 21
RAW MATERIALS USAGE TANK NUMBER: BEGIN OUTAGE: END OUTAGE: USAGE: NUMBER OF LIQUID BRINE TRUC NUMBER OF SALT TRUCKS UI NUMBER OF ACID TRUCKS UI NUMBER OF ACID RAILCARS	NLOADED: NLOADED: UNLOADED:				
TIME OF BATCHING PETRO PETRO USED IN BATCHING		Aliany	BATCHEL)	

REMARKS:

DATE: 12-8-11 LOT #: KII	-342	SFS OR PFS PRODUCTION [circle one]			
BOPERATOR: <u>54/114</u>		SHIFT: <u></u>			
/		SAMPLE	SAMPLE	SAMPLE	
1. TIME		07.35	0935	1135	
2. PRODUCTION RATE Start plant at 105 tpd and go to 120- tpd once - 325 < 10%	[tpd]	120	120	_ 110	
3. ACID [FSA] FLOW	[gpm]	50.4	50.5	41.1	
4. ACID [FSA] SPECIFIC GRAVITY		1230	1230	1230	
5. ACID [FSA] STRENGTH	%	25.670	25.6%	25.69	
6. KCL/SALT BRINE FLOW	[gpm]	<u>49.4</u>	49.4	40.0	
7. KCL/SALT BRINE SPECIFIC GRAVITY		1193	1150	_11.50	
8. COLOR OF BRINE		CIEAR	CRAR	CILAR	
(white, yellow, tan, brown) 9. COLOR OF ACID (white, yellow, tan, brown)		yellow	yellow	yell ou	
10. REACTOR NO. 1 TEMP [PFS ONLY]	[F]	<u>X</u>	<u> </u>	<u> </u>	
Maintain between 110 and 140 degrees 11. DRYER TEMPERATURE Maintain between 310 and 350 degrees	[F]	3500	351	367	
12. VACUUM READING Maintain between 12 and 18	["Hg]	12.5	13.5	12.5	
13. PRODUCT TEMPERATURE	[F]	25100	233'	300 +	
14. VENTURI SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 50 AND 55 gpm	[gpm]	50	50	50	
15. VENTURI SCRUBBER AIR PRESSURE AT INLET (POINT A)	["H20"]	10	_10	10	
16. VENTURI SCRUBBER AIR PRESSURE AT OUTLI [POINT B]	ET ["H20"]	3	2	_2	
17. VENTURI SCRUBBER DIFFERENTIAL PRESSUR [POINT A-B] Maintain between 8 and 14 inches of water	E ["H20"]	8			
18. WET SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 42 AND 47 gpm	[gpm]	<u>-4a</u>	_42	- 42	
19. WET SCRUBBER WATER PRESSURE MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	[psig]	21	_2]	_21	
20. WET SCRUBBER AIR PRESSURE AT INLET [POINT B]	["H2 0"]	_2		2	
21. WET SCRUBBER AIR PRESSURE AT OUTLET [POINT C]	["H20"]	<u>,5</u>	.5	<u> </u>	
22. WET SCRUBBER DIFFERENTIAL PRESSURE [POINT B-C] Maintain between 1.0 and 4.5 inches of water	["H20"]	1.5	1.5	1.5	
21. FRESH WATER TO REACTOR	[gpm]	X	X		
22. PETRO TO PRODUCT ON FILTER	[gpm]	3.5	3.5	3.5	
23. RINSE WATER TO PRODUCT ON FILTER	[gpm]	7.0	7.0	7.0	
PRODUCT SCREEN ANALYSIS		SAMPLE	SAMPLE	SAMPLE	
+60		-23	<u>, 43</u>	<u> </u>	
-	ld be less than 20]	<u> </u>	7.8	<u></u>	
	ld be less than 70]	50.0	55.6	<u>54.9</u>	
	ld be less than 30] Id be less than 10]	-2-1-2-	22.5	22.3	
-	-	1752	ويحمر والمؤام والألبات التروي أليا بالناوا بالمتحالة بيروا المتكاف المتعالما والمتعاد والمتعان	<u> </u>	
** If you are not able to maintain the above p			-	diately.	
Condition of Y-Strainer?: REMARKS:	Dia	you have to Clean i	L 5	a an an the subscript of the same the strategy of the subscript of the sub	

		KC INDUSTRIES, LLC. Y CONTROL AND PRODUCTION LOG					
date: <u>17/8/11</u>	LOT #: <u>K11-34</u> 2	2SFS	OR PFS PRODUCTION	N [circle one]			
A OPERATOR: <u>CHI</u>	ANCEN	SHI					
PRODUCT DRYING	START TIME:	1555 that product passes throug	STOP TIME: 6	2100			
	START TIME:	Na ngang tanàng kaominina mpikambana amin'ny kaodim-paositra dia mampikambana amin'ny kaodim-paositra dia mampikambana dia	STOP TIME:	autopolitonom, yöönekusta tillensen. Anvertet syönekusekunnekunn			
	START TIME:	an a	STOP TIME:	naadiinaa ahayaa ahaa ahaa ahayaa iina iina ahayaa ahayaa ahaa ahaa ahaa ahaa aha			
 FLOWS ON TIME FILTER START TIME FLOWS OFF TIME SCREWS DOWN TIME 		TIME 1 <u>1527</u> <u>1555</u> <u>2000</u> <u>2100</u>	<u>TIME 2</u>	TIME 3			
 TIME BURNER EXIT TEMP DRYER EXIT TEMP VENT FAN AMPS DRAFT FAN AMPS CHLORIDES 	161.	1655 N/A 377 25 70 17	1855 N/A 332 26 70 17				
DOWN TIMES AND REASON	19:	alahashdaan kohaa mada ya ahaa ka ahaa ka ahaa ka ahaa ahaa a	n an an Anna an Ann ann ann an Anna an A	۱۹۹۹ - ۲۰۰۹ کی			
RAW MATERIALS USAGE	I <u>FSA</u>		KCL				
TANK NUMBER:	<u> </u>	NEW STREAM ST	an a	Lating American States			
BEGIN OUTAGE :	2) - 4) "						
END OUTAGE:	5 10%	angenteenskopperatus Konning geferenskoppera					
USAGE: NUMBER OF LIQUID BRINE TR NUMBER OF SALT TRUCKS NUMBER OF ACID TRUCKS NUMBER OF ACID RAILCAR NUMBER OF KCL RAILCAR TIME OF BATCHING PETRO PETRO USED IN BATCHING	UNLOADED:	metoris _D 					
REMARKS:							

KC INDUSTRIES, LLC.

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× 1

DAILY QUALITY CONTROL AND PRODUCTION LOG (11, 24)

DATE: 12-8-11 LOT #: K11-342			SFS OR PFS PRODUCTION [circle one]				
BOPERATOR: Sordes			SHIFT:	200		ar alla a statica international and	
		SAMPLE	SA	AMPLE		SAMPLE	
1. TIME		1650		1850		-	
2. PRODUCTION RATE Start plant at 105 tpd and go to 120- tpd once - 325 < 10%	[tpd	/20		110			
3. ACID [FSA] FLOW	[gpn	n] <u>50</u>		48			
4. ACID [FSA] SPECIFIC GRAVITY		/233		1233			
5. ACID [FSA] STRENGTH	%	26%		201-			
6. KCL/SALT BRINE FLOW	[gpn	n] <u>49</u>		44			
7. KCL/SALT BRINE SPECIFIC GRAVITY		1201		1199			
8. COLOR OF BRINE [white, yellow, tan, brown]		1.48	. <u> </u>	hte_			
9. COLOR OF ACID [white, yellow, tan, brown]		<u></u>	-	YPIM			
10. REACTOR NO. 1 TEMP [PFS ONLY] Maintain between 110 and 140 degrees	[F]		•				
11. DRYER TEMPERATURE Maintain between 310 and 350 degrees	[F]	377	ہ <u>م</u> ینے	567			
12. VACUUM READING Maintain between 12 and 18	["Hį	d <u>/4</u>	•	/4			
13. PRODUCT TEMPERATURE	[F]	300*	0	276			
14. VENTURI SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 50 AND 55 gpm	E [gpr	n] <u>50</u>		50			
15. VENTURI SCRUBBER AIR PRESSURE AT I IPOINT A]	NLET ["H	20"]		10			
16. VENTURI SCRUBBER AIR PRESSURE AT O	OUTLET ["H2	20"] <u>2</u>		2			
[POINT B] 17. VENTURI SCRUBBER DIFFERENTIAL PRE	SSURE ["H	20"] _ <u>8</u>		8			
[POINT A-B] Maintain between 8 and 14 inches of water 18. WET SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 42 AND 47 gpm	[gpn	 ∧	n eginekin	42		da te alan yang karanga karang	
19. WET SCRUBBER WATER PRESSURE MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	[psig			<u>41</u>			
20. WET SCRUBBER AIR PRESSURE AT INLE? [POINT B]	["H2	20"]		2		- <u>11-11-11-11-11-11-11-11-11-11-11-11-11</u>	
21. WET SCRUBBER AIR PRESSURE AT OUTL [POINT C]	ET ["H2			: 5			
22. WET SCRUBBER DIFFERENTIAL PRESSUR [POINT B-C] Maintain between 1.0 and 4.5 inches of wate	-	20"] <u>/.5</u>		1.5			
21. FRESH WATER TO REACTOR	[gpr		•				
22. PETRO TO PRODUCT ON FILTER	[gpr	n] <u> </u>		4.0			
23. RINSE WATER TO PRODUCT ON FILTER	[gpr	n] <u>7.0</u>	1050 -	7.0	1950		
PRODUCT SCREEN ANALYSIS		SPAINE LES	DI DI	AMPLE		SAMPLE	
+60		.17	Constant of the International Constant States of the International Constant States of the International Constant	233	,17		
	Should be less that		12	12.9	9.3	and the second secon	
	Should be less that Should be less that			58.1	35.7 13.5		
	Should be less that [Should be less that			120.1 7.9	10.5	****	
** If you are not able to maintain the a							
Condition of Y-Strainer?: $\mathcal{O}_{\mathcal{T}}$		Did you have to C		~~ ~uu113 I	moundery	•	
REMARKS:							

na an a		INDUSTRIES, LLC.	DUCTION LO		DETRO
DATE: <u>12/12/11</u>	UDT #: <u>////</u>	LOT #: K11-346			DN [circle one]
A OPERATOR:	DOBSON / CHANCEY		SHIFT:	12/2	<u> </u>
PRODUCT DRYING	START TIME: [* defined as the time		es through the c	STOP TIME: Irying column]	2250
	START TIME:	escande outstatistical installant and chassed and an and an and	S Carry Statement	STOP TIME:	MULANY ZANTESASOKANY MANANANANANANANANANANANANANANANANANANAN
	START TIME:	diagong ang ang ang ang ang ang ang ang ang a		STOP TIME:	YET FLY YORM TO A DISA DISA DISA DISA DISA DISA DISA DI
		TIME 1	and the second	TIME 2	TIME 3
1. FLOWS ON TIME		1240			100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100
2. FILTER START TIME	3	135		eascital.ecocyclicte acceptantamesia.ecocyclicte	and the second statement of the second statement of the second statement of the second statement of the second
3. FLOWS OFF TIME		2230	Concert Without	VI (1996) - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1 9 :	and Protocology and the State of the State o
4. SCREWS DOWN TIM	1E	22.5	0	energia anti anti anti anti anti anti anti an	ander bit yzan transformatik ar da ander ande
5. TIME	n, na an	1450		1650	1850
6. BURNER EXIT TEMI		_N/A		NA	MA
7. DRYER EXIT TEMP		329	Auno Alvei en	345	369
8. VENT FAN AMPS		26		26	24
9. DRAFT FAN AMPS		70	anny Abita-	65	20
10. CHLORIDES		19.1	<u>D</u>	14.0	15.0
DOWN TIMES AND R	EASONS:		د در		
RAW MATERIALS US					
TANK NUM	IBER: <u>3</u>	40000075530000000000000000005553	anter all and the second s		
BEGIN OUT	AGE: <u>/'9"</u> HEL BALLY 2'0" USED	3 "			
END OUTA					Network Contractory
USAGE:	28"	alumanyou nangoonangan katalanganganganganganganganganganganganganga	۲۰٫۵۵٬۵۰۰ ۲۰۰۰ ۲۰۰۰ ۲۰۰۰ ۲۰۰۰ ۲۰۰۰ ۲۰۰۰ ۲۰۰	nten en directeren er	
NUMBER OF LIQUID BR	RINE TRUCKS UNLOADED	1			
NUMBER OF SALT TH	RUCKS UNLOADED:				
NUMBER OF ACID TR	RUCKS UNLOADED:	3			
NUMBER OF ACID RA	AILCARS UNLOADED:	0			
NUMBER OF KCL RA	ILCARS UNLOADED:	0			
TIME OF BATCHING	PETRO	$\overline{\mathbf{x}}$			
PETRO USED IN BATO	CHING	Δ			
REMARKS:		-			
SHAKER SCREEN CON	DITION AFTER LOADING TRA	ILER:	Descritting of the second s	20 (14 - 19 - 19 - 19 - 19 - 19 - 19 - 19 -	and a second

PRODUCTION TRAILER INTERNAL CONDITION AFTER UNLOADING:

DATE: 12-12-11 LOT #/ K	-346	~	PFS PRODUCTION	circle one]
BOPERATOR: Sylvia SAND	A section of the second section of the second section of the second section of the second second second second	- Ushi	61 017	
		SAMPLE	SAMPLE	SAMPLE
1. TIME	, <u>1999, 1997, 1997, 1997, 1997, 1997, 1997, 1997</u> , 19977, 1997, 1997, 1997, 1997, 1997, 1997, 1997, 1997, 1	1450	1050	1850
2. PRODUCTION RATE	[tpd]	90	90	98
Start plant at 105 tpd and go to 120- tpd once - 325 < 10%	r 7	285	28	38
3. ACID [FSA] FLOW	[gpm]	1200	2/	1227
4. ACID [FSA] SPECIFIC GRAVITY	A (JE U DA	254	Construction of the local division of the lo
5. ACID [FSA] STRENGTH	%	<u>23.7 10</u>		25.4
6. KCE/SALT BRINE FLOW	[gpm]	3515 119	$\frac{37}{100}$	7/
7. KCL/SALT BRINE SPECIFIC GRAVITY			1 1196 -119	10 -
8. COLOR OF BRINE		CRAR	Clear	<u>Clear</u>
[white, yellow, tan, brown] 9. COLOR OF ACID		Yellow	yella	yella
[white, yellow, tan, brown]			and the second	
10. REACTOR NO. 1 TEMP [PFS ONLY]	[F]	<u> </u>		
Maintain between 110 and 140 degrees 11. DRYER TEMPERATURE	[F]	371"	2 <i>6</i> ? °	373°
Maintain between 310 and 350 degrees	[*]			111
12. VACUUM READING	["Hg]	14	_/4	14
Maintain between 12 and 18 13. PRODUCT TEMPERATURE	[F]	243 "	280°	28/0
14. VENTURI SCRUBBER WATER FLOW RATE	[gpm]	50	50	50
MAINTAIN BETWEEN 50 AND 55 gpm	[81]			
15. VENTURI SCRUBBER AIR PRESSURE AT INLE	ET ["H20"]			
[POINT A] 16. VENTURI SCRUBBER AIR PRESSURE AT OUT	LET ["H2 0 "]	2	2	2
		3	8	B
17. VENTURI SCRUBBER DIFFERENTIAL PRESSU [POINT A-B] Maintain between 8 and 14 inches of water	RE ["H20"]			
18. WET SCRUBBER WATER FLOW RATE	[gpm]	42		42
MAINTAIN BETWEEN 42 AND 47 gpm	[maid]	21	21	21
19. WET SCRUBBER WATER PRESSURE MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	[psig]		and the construction of the sector and the sector of the s	
20. WET SCRUBBER AIR PRESSURE AT INLET	["H20"]	_2	_2	2
[POINT B]			7	5
21. WET SCRUBBER AIR PRESSURE AT OUTLET [POINT C]	["H20"]	2 لا	2	C.J.
22. WET SCRUBBER DIFFERENTIAL PRESSURE	["H20"]	1.5	1.5	1.5
[POINT B-C] Maintain between 1.0 and 4.5 inches of water	[]			
21. FRESH WATER TO REACTOR	[gpm]	X		X
22. PETRO TO PRODUCT ON FILTER	[gpm]	<u> </u>	X	<u> </u>
23. RINSE WATER TO PRODUCT ON FILTER	[gpm]	7.0	7.0	7,0
PRODUCT SCREEN ANALYSIS		SAMPLE	SAMPLE	SAMPLE
+60		213 d		9 .21
=	ould be less than 20]	4.9 9:	2 10.3 12.	in the second
-	ould be less than 70]	50.7 Cel		
•	ould be less than 30]	23.0 17	3 19.8 21.	
-	ould be less than 10]	10.6 5.	2 7.7 8.9	
** If you are not able to maintain the above				diately.
Condition of Y-Strainer?: 0/1	Did	l you have to Clean i	τι //ω	ta attai (1994). Ta i agaila ng ita agai ang ita agai attai na attai ang ita ang ita ang ita ang ita ang ita a
REMARKS:		a in the second seco		

Čtri v va v v			KC INDUSTRIES, LLC. DAILY QUALITY CONTROL AND PRODU				UCTION LO	DG	
DATE:	ate: <u>17/13/11</u> Lot #: <u>K11-3417</u>			347		SFS OR I	PFS PRODUCTIO	N [circle one]	
A OPER	ATOR:	DOBS	.cn)				SHIFT:	1.51	
PRODUCT DRYING		START TIN [* defined as			50 oduct passes	through the	STOP TIME:	1420	
			START TIN	IE:	**************************************	our we have the state of the state	384,6 7 ,	STOP TIME:	<u></u>
			START TIN	1E:	The state of the s	www.www.www.www.www.www.www.www.www.ww	NATION .	STOP TIME:	under zur den Kannen auf der Bereinen Mannen aus den Bereinen Mannen auf sich
2. FILTER	S ON TIME R START TIM S OFF TIME	1E				TIME 1 0623 0650 087	3 0 10	TIME 2 0950 0950 1405	<u>TIME 3</u>
4. SCREW	VS DOWN TI	ME				08	ZD	1420	MARKOWSKI KOMMANA ANTIKA MUTADA ANT
7. DRYEF 8. VENT	ER EXIT TEN R EXIT TEMI FAN AMPS T FAN AMPS ORIDES					0750 N/H 348 34 70 260	<u></u>	1050 NIA 369° 24 70 11	1750 W/A 386° 24 70 7.3
DOWN T	IMES AND I	REASONS:	* SHUT BAD	Doll	NN Z	UE TO	o For,	<u>VAWE</u>	1 n)
RAW MA	TERIALS U	SAGE							
	TANK NU	MBER:	H	<u>FSA</u>			and the state of the	<u>KCL</u>	Januar Talan Jalang Man
	BEGIN OL	TAGE:	_/		an a				an a
	END OUT.	AGE:	3'3'/2"		Barranda and a standard and a standard and a standard a standard a standard a standard a standard a standard a				
	USAGE:		27 1/2"		Characteristic and the second s	a-jacka 2004/04	57757074598 compEter 3355700009258 com	SAFIN Altanus/Arrow	
NUMBEI NUMBEI NUMBEI NUMBEI TIME OF	R OF SALT T R OF ACID T R OF ACID F	TRUCKS UI TRUCKS UI RAILCARS AILCARS I G PETRO				- - - Milm	DY BAR		
REMARI	KS:								

	347 *	STO UK I	PFS PRODUCTION	[circle one]
BOPERATOR: <u>Sylvia</u>		SHIF	T: 1 ⁵⁺	
		SAMPLE	SAMPLE	SAMPLE
1. TIME		015D	1050	1250
2. PRODUCTION RATE Start plant at 105 tpd and go to 120- tpd once - 325 < 10%	[tpd]	120	115	120
3. ACID [FSA] FLOW	[gpm]	51.5	48.5	51.5
4. ACID [FSA] SPECIFIC GRAVITY		1226	1226	1226
5. ACID [FSA] STRENGTH	%	<u>25,259</u> 0	25.25%	25.257
6. KCL/ SALT BRINE FLOW	[gpm]	48.2	46.1	48.1
7. KCL/ SALT BRINE SPECIFIC GRAVITY		<u></u>	1186	1133
8. COLOR OF BRINE		Clear	CLEAR	LICAR
[white, yellow, tan, brown] 9. COLOR OF ACID [white, yellow, tan, brown]		yellow	yellow	yellow
10. REACTOR NO. 1 TEMP [PFS ONLY] Maintain between 110 and 140 degrees	[F]	<u> </u>	_X	_X
11. DRYER TEMPERATURE Maintain between 310 and 350 degrees	[F]	<u>371°</u>	<u>342°</u>	386
12. VACUUM READING Maintain between 12 and 18	["Hg]	12.5	13.0	13.0
13. PRODUCT TEMPERATURE	[F]	297°	261	291
14. VENTURI SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 50 AND 55 gpm	[gpm]	<u>.50</u>	50	50
15. VENTURI SCRUBBER AIR PRESSURE AT INLET [POINT A]	["H20"]	_10		<u> </u> ⊅
16. VENTURI SCRUBBER AIR PRESSURE AT OUTLET [POINT B]	["H20"]	_2	_2	_2
17. VENTURI SCRUBBER DIFFERENTIAL PRESSURE [POINT A-B] Maintain between 8 and 14 inches of water	["H20"]	8	8	
18. WET SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 42 AND 47 gpm	[gpm]	42	<u>42</u>	42
19. WET SCRUBBER WATER PRESSURE MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	[psig]		21	21
20. WET SCRUBBER AIR PRESSURE AT INLET [POINT B]	["H20"]			2
21. WET SCRUBBER AIR PRESSURE AT OUTLET [POINT C]	["H20"]	·5	.5	15
22. WET SCRUBBER DIFFERENTIAL PRESSURE [POINT B-C] Maintain between 1.0 and 4.5 inches of water	["H20"]	1.5	1.5	1.5
21. FRESH WATER TO REACTOR	[gpm]	×	×	X
22. PETRO TO PRODUCT ON FILTER	[gpm]	3.5	3.5	3.5
23. RINSE WATER TO PRODUCT ON FILTER	[gpm]	7.0	7.0	7.0
PRODUCT SCREEN ANALYSIS		SAMPLE	SAMPLE	SAMPLE
+60		.12	.25	
-	be less than 20]	8.3	10.4	10,6
-	be less than 70]	50.7	53.8	6.7
	be less than 30]	22.9	20.8	18.0
-	be less than 10]	16.8	13.9	8.7
** If you are not able to maintain the above par				diately.
Condition of Y-Strainer?: REMARKS:	Dia	you have to Clean it	5 	a an

DAILY QUALITY CONTROL AND PRODUCTION LOG								
DATE: 12-13-11	LOT #: <u>()(-</u>	347	SFS OR P	FS PRODUCTIO	ON [circle one]			
A OPERATOR: <u>CHAA</u>	СЕЦ		SHIFT:	2 nd				
PRODUCT DRYING	/ START TIME: [* defined as the time	period that product passes	through the d	STOP TIME:	1830			
	START TIME:	_1925	_	STOP TIME:	2135			
	START TIME:		-	STOP TIME:				
		TIME 1		TIME 2	TIME 3			
1. FLOWS ON TIME		1630		1920				
2. FILTER START TIME		1650	_	1925	100-100-100-100-100-100-100-100-100-100			
3. FLOWS OFF TIME		1830		2120				
4. SCREWS DOWN TIME		1830	_	2135				
5. TIME		1750		1950				
6. BURNER EXIT TEMP		NA		a de a para a para de a para de a partes de a partes	ay tanya da katang manganang sa katang s			
7. DRYER EXIT TEMP		370		ani, dhang maratik Sala. Thian ta dalla in				
8. VENT FAN AMPS		24						
9. DRAFT FAN AMPS		<u>סר</u>						
10. CHLORIDES		¥.1	fing .	angitantani ing kaging t	ected/actioncome.onity/confictional/confi			

KC INDUSTRIES, LLC.

DOWN TIMES AND REASONS:	down de	in to class	Juin 1. p. s.	sturrare.	1830-1920	
Ba			vine 1885 -		·	

RAW	MA	TERIALS	USAGE

			<u>FSA</u>		KC	ſ.
	TANK NUMBER:	4	<u></u>	Scout for This Philipping and the state		62570/8270/8270/82970/82970/82970/82970/82970
	BEGIN OUTAGE:	3'3'/2'`				
	END OUTAGE:	4'6"				
	USAGE:	14 1/2"				
NUMBER	OF LIQUID BRINE TRU	ICKS UNLOADE	D	<u>_@</u>		
NUMBE	R OF SALT TRUCKS U	JNLOADED:		1		
NUMBE	R OF ACID TRUCKS U	JNLOADED:				
NUMBE	R OF ACID RAILCAR	S UNLOADED:		X		
NUMBE	R OF KCL RAILCARS	UNLOADED:		Ø		
TIME O	F BATCHING PETRO			15:40		
PETRO	USED IN BATCHING			1/2 BAG		
	7 20.					

REMARKS:

SHAKER SCREEN CONDITION AFTER LOADING TRAILER: Govel. PRODUCTION TRAILER INTERNAL CONDITION AFTER UNLOADING: 3-4 Tons STUCK on Sides

DATE: <u>12-13-11</u> LOT #: <u>411</u>	GES OR PFS PRODUCTION [circle one]			
BOPERATOR: Sarders	an Marina ang Kinggina yang Kanggina yang Kanang	SHI	FT: <u>2°9</u>	
		SAMPLE	SAMPLE	SAMPLE
1. TIME		1759	2100	
2. PRODUCTION RATE Start plant at 105 tpd and go to 120- tpd once - 325 < 10%	[tpd]	120	100	END-HOLESCOVIESCOVIESCOVIES
3. ACID [FSA] FLOW	[gpm]	31	43	
I. ACID [FSA] SPECIFIC GRAVITY		1.226	1220	
. ACID [FSA] STRENGTH	%	25.25%	1525	i ya nga kana nga kata kana na palingan sa kana kana kana kana kana kana kana
5. KCL/SALT BRINE FLOW	[gpm]	47	39	djangag kapana na bajda man da karana Tari na gan
. KCL/SALT BRINE SPECIFIC GRAVITY		1160	1100	Accession and the second states of the second state
COLOR OF BRINE		white	inh. HC	
white, yellow, tan, brown] D. COLOR OF ACID		usella	yella-	
vhite, yellow, tan, brown]		<u></u>	-fene-	المريخ متي الرابع من المريجين بين المريجين
0. REACTOR NO. 1 TEMP [PFS ONLY]	[F]			The second second frances
Asintain between 110 and 140 degrees	f m 1	366	278.	
11. DRYER TEMPERATURE Aaintain between 310 and 350 degrees	[F]	<u></u>	570	
2. VACUUM READING	["Hg]	13	13	
laintain between 12 and 18	L03	100	105	
3. PRODUCT TEMPERATURE	[F]	299	285	
4. VENTURI SCRUBBER WATER FLOW RATE	[gpm]	50	50	
IAINTAIN BETWEEN 50 AND 55 gpm .5. VENTURI SCRUBBER AIR PRESSURE AT INLET	["H20"]	12	12	
		2)	
6. VENTURI SCRUBBER AIR PRESSURE AT OUTLE" [POINT B]	Г ["Н20"]	<u> </u>		
7. VENTURI SCRUBBER DIFFERENTIAL PRESSURE	["H20"]	10 .	10	
[POINT A-B] Maintain between 8 and 14 inches of water	[amm]	42	117	
8. WET SCRUBBER WATER FLOW RATE AINTAIN BETWEEN 42 AND 47 gpm	[gpm]	ethantik antikanak analisis	- 1	
9. WET SCRUBBER WATER PRESSURE	[psig]	_21	21	
IAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	FUT 7- AU	9	2	
(0. WET SCRUBBER AIR PRESSURE AT INLET [POINT B]	["H20"]			
21. WET SCRUBBER AIR PRESSURE AT OUTLET	["H20"]	5	.5	
[POINT C]			e and an and a second	
2. WET SCRUBBER DIFFERENTIAL PRESSURE	["H2 0 "]	1.5	1.5	\$1442471004700040000440004400044
[POINT B-C] Maintain between 1.0 and 4.5 inches of water	[
11. FRESH WATER TO REACTOR	[gpm]	4.0		
2. PETRO TO PRODUCT ON FILTER	[gpm]		4.9	
3. RINSE WATER TO PRODUCT ON FILTER	[gpm]	7.0	<u> </u>	
PRODUCT SCREEN ANALYSIS		SAMPLE	SAMPLE	SAMPLE
+60		<u>= 12</u>		
-	1 be less than 20] 1 be less than 70]	10.2	9.6	
-	t be less than 30]	20.1	17.9	
	i be less than 10]	5.9	3.6	
** If you are not able to maintain the above pa	_			diately.
ondition of Y-Strainer?: Oh		you have to Clean i	•	•

		C INDUSTRIES, LL CONTROL AND P		LOG STALL	5-1255
DATE: 17/14/11	LOT #:	11-348	(SFS O	R PFS PRODUCTION	I [circle one]
A OPERATOR: DOB	son)		SHIFT	:	
PRODUCT DRYING	START TIME: [* defined as the tim	e period that product p	basses through t	STOP TIME:	0850
	START TIME:	0950		STOP TIME:	1528
	START TIME:	Participante de la constante d	COMPANY REPORT OF STREET, MILLIN	STOP TIME:	a sa ang ang ang ang ang ang ang ang ang an
		TIM	<u>E 1</u>	TIME 2	TIME 3
1. FLOWS ON TIME		O_{i}	814	an protocol de comenciación de la c	water and a standard
2. FILTER START TIME		_0_	840	energiesellowy our tijder sometider	400589925777777442035940196698698699494594
3. FLOWS OFF TIME		_15	15	€.http://www.commerciality.com/interaction/commerciality.com	ugy franzonen an interne alfa Chandheim Billinger, anne
4. SCREWS DOWN TIME			78		BLEN LEY MINISTER OF THE OFFICE OF THE OFFICE OFFICE
5. TIME	<u>anna ann an amhraig ann an ann ann an ann an ann an ann an</u>	Ð	940	1140	1340
6. BURNER EXIT TEMP			NA	NA	N/H
7. DRYER EXIT TEMP			45"	<u>300°</u>	352"
8. VENT FAN AMPS		3	23_	_23_	<u> </u>
9. DRAFT FAN AMPS			<u>e q</u>	- Certa	69
10. CHLORIDES		21,	D	16.0	16.0
DOWN TIMES AND REASONS	: ¥ SHUT	DOWNJUZ	TO Fil	TRATE C F	UTER PHUSS
RAW MATERIALS USAGE	1910 A				
TANK NUMBER:	<u></u>		National Relationships	<u>KCL</u>	N2A48T-362T0320HH+
BEGIN OUTAGE:	1'4'	والمراحقين فالمراجع من المراجع	CONTRACTOR OF THE OWNER		ning dan kanalan
END OUTAGE:	3'7"	والم المراحلة المراجلة المراجلة في المراجلة المراجلة المراجلة المراجلة المراجلة المراجلة المراجلة المراجلة الم المراجلة المراجلة الم			
USAGE:	27"	475500000000000000000000000000000000000	مىسىلىكى مەرىپى بىرىكى بىرىمىيى بىرىكى بىرىمىيى بىرىكى بىرىمىيى بىرىكى بىرىمىيى بىرىكى بىرىمىيى بىرىكى بىرىكى ب بىرىمىيەر بىرىرى بىرىمى بىرىكى بىرىمىيى بىرىكى بىرىمىيى بىرىكى بىرىمىيى بىرىكى بىرىمىيى بىرىكى بىرىمىيى بىرىكى ب		
NUMBER OF LIQUID BRINE TRU	CKS UNLOADED	Ø			
NUMBER OF SALT TRUCKS U	INLOADED:	Ø			
NUMBER OF ACID TRUCKS U	INLOADED:	3			
NUMBER OF ACID RAILCARS	S UNLOADED:	0			
NUMBER OF KCL RAILCARS	UNLOADED:	0			
TIME OF BATCHING PETRO		2300. ON	12/141	121	
PETRO USED IN BATCHING		1/2			
REMARKS:					

DATE: <u>12-14-11</u> LOT#: <u>K11-</u> BOPERATOR: <u>Sylvia Sanders</u>	348	L /			
in the first in th		$\underbrace{\text{SFS OR PFS PRODUCTION [circle one]}}_{\text{SHIFT:}} \frac{3T}{2^{NO}}$			
· · · · · · · · · · · · · · · · · · ·		SAMPLE	SAMPLE	SAMPLE	
1. TIME		0940	1140	1340	
2. PRODUCTION RATE Start plant at 105 tpd and go to 120- tpd once - 325 < 10%	[tpd]	120	120	120	
3. ACID [FSA] FLOW	[gpm]	51.5	51.6	51.2	
4. ACID [FSA] SPECIFIC GRAVITY		1225	1225	1225	
5. ACID [FSA] STRENGTH	%	25.3%	25.3%	25.17	
6. KCD/SALT BRINE FLOW	[gpm]	48.1	46.7	49.4	
7. KCL/ SALT BRINE SPECIFIC GRAVITY	LOF	1195	1194	1194	
8. COLOR OF BRINE		CLEAR	CLEME	CLEAR	
white, yellow, tan, brown]		5 Å		<u>Sterio</u>	
9. COLOR OF ACID white, yellow, tan, brown}		yellow	Yellow	yellow	
10. REACTOR NO. 1 TEMP [PFS ONLY] Maintain between 110 and 140 degrees	[F]	<u> </u>	<u>X</u>	<u> </u>	
11. DRYER TEMPERATURE Maintain between 310 and 350 degrees	[F]	352	360	372	
12. VACUUM READING Maintain between 12 and 18	["Hg]	12.5	<u>14.0</u>	14.0	
13. PRODUCT TEMPERATURE	[F]	216	282	267	
14. VENTURI SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 50 AND 55 gpm	[gpm]	52	50	50	
15. VENTURI SCRUBBER AIR PRESSURE AT INLET [POINT A]	["H20"]	11.5	<u>_11.s</u>	11.5	
16. VENTURI SCRUBBER AIR PRESSURE AT OUTLET [POINT B]	["H20"]	2	<u></u>		
7. VENTURI SCRUBBER DIFFERENTIAL PRESSURE [POINT A-B] Maintain between 8 and 14 inches of water	["H20"]	9.5	9.5	9.5	
18. WET SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 42 AND 47 gpm	[gpm]	43	<u>Ча</u>	42	
19. WET SCRUBBER WATER PRESSURE MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	[psig]	21	<u>_21</u>	21	
20. WET SCRUBBER AIR PRESSURE AT INLET [POINT B]	["H20"]	_2	2	2	
21. WET SCRUBBER AIR PRESSURE AT OUTLET [POINT C]	["H20"]	•5	-5	.5	
22. WET SCRUBBER DIFFERENTIAL PRESSURE	["H20"]	1.5	1.5	1.5	
[POINT B-C] Maintain between 1.0 and 4.5 inches of water					
21. FRESH WATER TO REACTOR	[gpm]	×			
22. PETRO TO PRODUCT ON FILTER	[gpm]	3,5	3.5	3.5	
23. RINSE WATER TO PRODUCT ON FILTER	[gpm]	7.0	7.0	7.0	
PRODUCT SCREEN ANALYSIS		SAMPLE	SAMPLE	SAMPLE	
+60		.19	.16	.15	
	be less than 20]	8.6	7.9	9.3	
	be less than 70]	37.	52.5	57.0	
-	be less than 30]	21.4	26.0		
	be less than 10]	31.6	13.0	9.2	
** If you are not able to maintain the above para	-	-		diately.	
Condition of Y-Strainer?:	Did	l you have to Clean i	t?		

general da		INDUSTRIES, LLC.	UCTION LOG	ŕ	
DATE: <u>[2-14-1]</u>	LOT #: <u> ///·</u>	348	SFS OR PF	S PRODUCTION	[circle one]
A OPERATOR: <u>CHAN</u>	Icey		SHIFT:	Znd	
PRODUCT DRYING	START TIME: [* defined as the time				2143
	START TIME:	• • •		STOP TIME:	
	START TIME:			STOP TIM <u>E:</u>	
 FLOWS ON TIME FILTER START TIME FLOWS OFF TIME SCREWS DOWN TIME 		TIME 1 /715 1735 2130 2143	, 	ГIME 2	TIME 3
 TIME BURNER EXIT TEMP DRYER EXIT TEMP VENT FAN AMPS DRAFT FAN AMPS CHLORIDES 		/835 N/A 366 23 70 6.0		2035 N/A 367 23 68 19.0	
DOWN TIMES AND REASONS:					
RAW MATERIALS USAGE	/ FSA		*****	KCL	******
TANK NUMBER:					
BEGIN OUTAGE:	1'3"			_	
END OUTAGE:	2'81/2"				
USAGE:	<u>וי בן' רן '</u>	······································			
BETAE TWOKS NUMBER OF SALT TRUCKS U NUMBER OF ACID TRUCKS U NUMBER OF ACID RAILCARS NUMBER OF KCL RAILCARS TIME OF BATCHING PETRO PETRO USED IN BATCHING REMARKS: SHAKER SCREEN CONDITION A	NLOADED: UNLOADED: UNLOADED:	 			
		2-3 TM	s stru	Con Sides	OF K-7

B OPERATOR: Select SHIFT: 2^{-24} SAMPLE SAMPLE SAMPLE SAMPLE SAMPLE SAMPLE SAMPLE SAMPLE 1. TIME $/335$ 3035 3035 2. PRODUCTION RATE [tpd] $/2.0$ $/10^{-0}$ Start plant at 105 tpd and go to 120- tpd once - 325 < 10%	DATE: 12-14-11 LOT #: KI	11-348	_ SFOR	PFS PRODUCTION	circle one]
1. TIME $1 \cdot 1 \cdot$	BOPERATOR: Saded	an a chuir an tha an a chuir a' chuir chuir chuir a chuir	SHI	FT: <u>222</u>	ne des salations de la company de la comp
2. PRODUCTION RATE[tpd] $/2.0$ $/1.0$ 2. PRODUCTION RATE[tpd] $/2.0$ $/1.0$ 2. Starplant at 105 (pd and go to 120: (pd once -325 < 10%)[gpm] $/2.0$ $/1.0$ 3. ACID [FSA] FLOW[gpm] 52 52 $/2.0$ 4. ACID [FSA] SPECIFIC GRAVITY $/2.01$ $/1.021$ $/1.021$ 5. ACID [FSA] STRENGTH% 24.75 24.75 24.75 6. KCL/SALT BRINE FLOW[gpm] 49 49 79 7. KCL/SALT BRINE SPECIFIC GRAVITY[gpm] 49 49 8. COLOR OF BRINE 44.76 44.76 44.76 9. COLOR OF ACID 44.76 44.76 44.76 9. COLOR OF BRINE[F] 37.5^{-1} 44.76 9. COLOR OF BRINE[F] 37.5^{-1} 44.76 9. COLOR OF BRINE[F] 37.5				SAMPLE	SAMPLE
as a track 105 bit and go to 120- bit once - 325 < 10%(14-3) 12 3. ACID [FSA] FLOW[gpm] 52 52 4. ACID [FSA] SPECIFIC GRAVITY $1221 - 1$ 1221 5. ACID [FSA] STRENGTH% 247.75 247.75 6. KCL/SALT BRINE FLOW[gpm] 49 $1135 - 1135$ 7. KCL/SALT BRINE SPECIFIC GRAVITY $1129 - 1135 - 1135$ $1135 - 1135$ 8. COLOR OF BRINE $447 - 1135 - 1135$ $1135 - 1135$ 9. COLOR OF BRINE $447 - 1135 - 1135$ $447 - 1135 - 1135$ 9. COLOR OF ACID $447 - 1135 - 1135$ $447 - 1135 - 1135$ 10. REACTOR NO. 1 TEMP [PFS ONLY][F] 370° 11. DRYER TEMPERATURE[F] 370° 12. VACUUM READING["Hg] $14 - 144$ Maintain between 110 and 1360 degrees["Hg] $14 - 144$ 13. PRODUCT TEMPERATURE[F] 230° 13. PRODUCT TEMPERATURE[F] 230° 13. PRODUCT TEMPERATURE[F] 230° 13. PRODUCT TEMPERATURE[F] 230° 14. PRODUCT TEMPERATURE[F] 230° 15. PRODUCT TEMPERATURE[F] 230° 16. READING["Hg] $144 - 144 -$	1. TIME		Contraction of the Contraction of Contract	3035	والمراجع والمراجع والمراجع والمراجع والمراجع والمراجع
3. ACID [FSA] FLOW [gpm] 52 52 4. ACID [FSA] SPECIFIC GRAVITY		[tpd]	120	12	and a constant of the first of the part of
4. ACID [FSA] SPECIFIC GRAVITY $121 - 1$ 121 5. ACID [FSA] STRENGTH % 24.75 24.75 6. KCL/SALT BRINE FLOW [gpm] 49 47 7. KCL/SALT BRINE SPECIFIC GRAVITY $1129 - 1135 - 1135$ $1135 - 1135$ 8. COLOR OF BRINE $1129 - 1135 - 1135$ $1135 - 1135$ 9. COLOR OF ACID $1129 - 1135 - 1135$ $110 - 110 - 1100$ 9. COLOR OF ACID $110 - 110 - 1100$ $110 - 110 - 1100$ 9. COLOR OF ACID $110 - 110 - 1100$ $110 - 110 - 1100$ 9. COLOR OF ACID $110 - 110 - 1100$ $110 - 110 - 1100$ 9. COLOR OF ACID $110 - 110 - 1100$ $110 - 110 - 1100$ 9. COLOR OF ACID $110 - 110 - 1100$ $110 - 1100 - 1100$ 9. COLOR OF ACID $110 - 110 - 1100 - 1100$ $110 - 1100 - 1100 - 11000$ 9. COLOR OF ACID $110 - 110 - 1100 - 11000$ $110 - 1100 - 11000 - 11000$ 9. COLOR OF ACID $110 - 1100 - 11000 - 110000$ $110 - 11000 - 11000000$ 9. COLOR OF ACID $110 - 110000000000000000000000000000000$		[gpm]	52	52	
5. ACID [FSA] STRENGTH % <u>24.75</u> <u>24.74</u> 6. KCL/SALT BRINE FLOW [gpm] <u>49</u> <u>49</u> 7. KCL/SALT BRINE SPECIFIC GRAVITY [J129] [J135]			1221-1	1221	
6. KCL/SALT BRINE FLOW [gpm] <u>49</u> <u>49</u> 7. KCL/SALT BRINE SPECIFIC GRAVITY <u>1129</u> <u>1135</u> <u>1135</u> 8. COLOR OF BRINE <u>white</u> <u>white</u> <u>white</u> <u>white</u> [white, yellow, tan, brown] <u>yellow</u> <u>yellow</u> <u>yellow</u> 9. COLOR OF ACID <u>yellow</u> <u>yellow</u> <u>yellow</u> (write, yellow, tan, brown] [F] <u>yellow</u> <u>yellow</u> 10. REACTOR NO. 1 TEMP [PFS ONLY] [F] <u>yellow</u> <u>yellow</u> 11. DRYER TEMPERATURE [F] <u>379</u> ⁵ <u>375</u> ⁵ 12. VACUUM READING ["Hg] <u>/4</u> <u>/4</u> Maintain between 310 and 350 degrees ["Hg] <u>/4</u> <u>/4</u> 13. PRODUCT TEMPERATURE [F] <u>280</u> [*] <u>288</u> [*]		%	24.75	24.75	
8. COLOR OF BRINE utile utile <td></td> <td>[gpm]</td> <td>49</td> <td>49</td> <td></td>		[gpm]	49	49	
8. COLOR OF BRINE utile utile <td>7. KCL/SALT BRINE SPECIFIC GRAVITY</td> <td></td> <td>1129 - 113</td> <td>5 - 1135</td> <td></td>	7. KCL/SALT BRINE SPECIFIC GRAVITY		1129 - 113	5 - 1135	
9. COLOR OF ACID yellow yel			juste	white	
[white, yellow, tan, brown] [F]	· · · · · · · · · · · · · · · · · · ·		wolla	uslla	
Maintain between 110 and 140 degrees [F] 370° 375° 11. DRYER TEMPERATURE [F] 370° 375° Maintain between 310 and 350 degrees ["Hg] 14 14 12. VACUUM READING ["Hg] 14 14 Maintain between 12 and 18 [F] 290° 248° 13. PRODUCT TEMPERATURE [F] 290° 268°			<u>-700</u>	-if the second s	andre to an
11. DRYER TEMPERATURE [F] 372 375 Maintain between 310 and 350 degrees ["Hg] 14 14 12. VACUUM READING ["Hg] 14 14 Maintain between 12 and 18 [F] 290° 248° 13. PRODUCT TEMPERATURE [F] 290° 268°		[F]		Completion Contraction Contraction	
Maintain between 310 and 350 degrees ["Hg] 14 14 12. VACUUM READING ["Hg] 14 14 Maintain between 12 and 18 [F] 280° 288° 13. PRODUCT TEMPERATURE [F] 280° 268°		ſFÌ	370	375'	
Maintain between 12 and 18 13. PRODUCT TEMPERATURE [F] 230° 233°	Maintain between 310 and 350 degrees		121	/ L/	
		["Hg]	17	17	
	13. PRODUCT TEMPERATURE	[F]	280	288	فالمترك والمحافظ والم
14. VENTURI SCRUBBER WATER FLOW RATE [gpm] <u>50</u> <u>50</u>	14. VENTURI SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 50 AND 55 gpm	[gpm]	50	_50	The Print of the Print P
15. VENTURI SCRUBBER AIR PRESSURE AT INLET ["H20"] <u>12</u> <u>12</u>	15. VENTURI SCRUBBER AIR PRESSURE AT INLE	T ["H20"]	12	12	
[POINT A] 16. VENTURI SCRUBBER AIR PRESSURE AT OUTLET ["H20"] 2	16. VENTURI SCRUBBER AIR PRESSURE AT OUTI	LET ["H20"]	_2	2	
[POINT B] 17. VENTURI SCRUBBER DIFFERENTIAL PRESSURE ["H20"]		RE ["H20"]	10	10	
[POINT A-B] Maintain between 8 and 14 inches of water 18. WET SCRUBBER WATER FLOW RATE [gpm] 4/2 4/2			40	40	
MAINTAIN BETWEEN 42 AND 47 gpm	MAINTAIN BETWEEN 42 AND 47 gpm			12	
MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE		[psig]		<u> </u>	
20. WET SCRUBBER AIR PRESSURE AT INLET ["H20"] 2 2		["H20"]	2	<u> </u>	
21. WET SCRUBBER AIR PRESSURE AT OUTLET ["H20"] <u>.5</u> .5		["H20"]	<u>.5</u>	: 5	
22. WET SCRUBBER DIFFERENTIAL PRESSURE ["H20"] /.5		["H20"]	1.9	1.5	
21. FRESH WATER TO REACTOR [gpm]	21. FRESH WATER TO REACTOR	[gpm]			
22. PETRO TO PRODUCT ON FILTER [gpm] <u>4.0</u> <u>4.9</u>	22. PETRO TO PRODUCT ON FILTER	[gpm]	energeneration	The state of the s	Contraction of the second s
23. RINSE WATER TO PRODUCT ON FILTER [gpm] <u>6.9</u> <u>6.9</u>	23. RINSE WATER TO PRODUCT ON FILTER	[gpm]	6.0	6.0	415 771795784577958457755277552775527755277552
PRODUCT SCREEN ANALYSIS SAMPLE SAMPLE SAMPLE					SAMPLE
+60 +100 [Should be less than 20] $\frac{22}{1^{2}.6}$ $\frac{17}{11.3}$		uld be less than 20]	وأجري والمتحد والجادي وجريسة المتحالة المتحالة المتحالة والمحالة والمحالة والمحالة والمحالة		
+100 [Should be less than 20] $1^{2}.4$ 11.3 11.6 +200 [Should be less than 70] 65.1 63.4	E	-			
+325 [Should be less than 30] $/\beta_{\cdot}\beta_{\cdot}$ // $\beta_{\cdot}\beta_{\cdot}$ // $\beta_{\cdot}\beta_{\cdot}$				9 17.1	
-325 [Should be less than 10] (a, D) 7.4 (a, da)		-		A lada	
** If you are not able to maintain the above parameters, you should contact Terry Connelly or Dean Qualls immediately.	** If you are not able to maintain the above	parameters, you should	contact Terry Conn	elly or Dean Qualls imme	diately.
Condition of Y-Strainer?: OH Did you have to Clean it? NO REMARKS:		Did	you have to Clean i	t? <u>10</u>	

al and a	KC INDUS DAILY QUALITY CONTR	STRIES, LLC. OL AND PRODUCTION L	.0G	
DATE: <u>17/15/11</u>	LOT #: <u></u>		PFS PRODUCTIO	N [circle one]
A OPERATOR:	rson	SHIFT:	155	
PRODUCT DRYING	START TIME: [* defined as the time period t	Db15 hat product passes through the	STOP TIME: drying column]	1350
	START TIME:	water and the state of the stat	STOP TIM <u>E:</u>	alan sa ka
	START TIME:		STOP TIME:	ekang at waterat di eksetatu di esert atas da katera kan tekna kan sa
		TIME 1	TIME 2	TIME 3
 FLOWS ON TIME FILTER START TIME FLOWS OFF TIME SCREWS DOWN TIME 		0418 0445 1730 1350		
 5. TIME 6. BURNER EXIT TEMP 7. DRYER EXIT TEMP 8. VENT FAN AMPS 9. DRAFT FAN AMPS 10. CHLORIDES 		0745 N/A 344* 23 70 26	0945 N/A 381° 23 70 5.5	1145 N/A 270° 70 2.3
DOWN TIMES AND REASO	NS:			
RAW MATERIALS USAGE	TICLA		87 (1) 1	
TANK NUMBER:	<u>FSA</u>		<u>KCL</u>	01-10-11-11-11-11-11-11-11-11-11-11-11-1
BEGIN OUTAGE:	1'5"			
END OUTAGE:	3'7"	nangkananapilan dapaten magalananapilan Manahananan magalanahan magalana katalanan		
USAGE:	26"			
NUMBER OF LIQUID BRINE TO NUMBER OF SALT TRUCKS NUMBER OF ACID TRUCKS NUMBER OF ACID RAILCA NUMBER OF KCL RAILCA TIME OF BATCHING PETRO PETRO USED IN BATCHING REMARKS: SHAKER SCREEN CONDITIO	S UNLOADED:	0 0 230 /Z		

'n

PRODUCTION TRAILER INTERNAL CONDITION AFTER UNLOADING:

DATE: 12-15-11 LOT #: K11-349			SFS OR PFS PRODUCTION [circle one] SHIFT: 1 ^{5†}			
BOPERATOR: <u>Sylvia</u>	991107710001100010007000010000700011000000					
. TIME			SAMPLE 0155	SAMPLE 0955	<u>SAMPLE</u> 1155	
		[tmd]	120	120	//0	
PRODUCTION RATE tart plant at 105 tpd and go to 120- tpd once - 325 < 10%		[tpd]	$1 \propto \nu$	180		
. ACID [FSA] FLOW		[gpm]	52.3	52.1	39	
ACID [FSA] SPECIFIC GRAVITY			1221	1221	1221	
. ACID [FSA] STRENGTH		%	24.7.5%	24.75%	<u> </u>	
. KCL /SALT BRINE FLOW		[gpm]	49.6	48.3	40.3	
. KCL/ SALT BRINE SPECIFIC GRAVIT	Y		1200	1126	1145	
COLOR OF BRINE			white	white	WHITE	
hite, yellow, tan, brown] • COLOR OF ACID hite, yellow, tan, brown]	м. 		yellow	yellow	_ yellon	
0. REACTOR NO. 1 TEMP [PFS ONLY]		[F]	×	'X	Í X	
laintain between 110 and 140 degrees		f- 1		- 0		
1. DRYER TEMPERATURE laintain between 310 and 350 degrees		[F]	366	3810	3700	
2. VACUUM READING aintain between 12 and 18		["Hg]	12.0	14.0	13.0	
3. PRODUCT TEMPERATURE		[F]	276°	293	7.70	
4. VENTURI SCRUBBER WATER FLOV AINTAIN BETWEEN 50 AND 55 gpm	W RATE	[gpm]	50	50	50	
5. VENTURI SCRUBBER AIR PRESSUI	RE AT INLET	{"H20"}	10	_1 <i>D</i>	10-0	
[POINT A] 6. VENTURI SCRUBBER AIR PRESSUR	RE AT OUTLET	["H20"]	2	_2	2.0	
(POINT B] 7. VENTURI SCRUBBER DIFFERENTL	AL PRESSURE	["H2O"]	Q	0	7.0	
[POINT A-B] Maintain between 8 and 14 inches		[
8. WET SCRUBBER WATER FLOW RA AINTAIN BETWEEN 42 AND 47 gpm	TE	[gpm]	42	<u>4a</u>		
9. WET SCRUBBER WATER PRESSUR AINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRA		[psig]	_2]	_21		
0. WET SCRUBBER AIR PRESSURE AT [POINT B]	FINLET	["H20"]	<u></u>	_2	7.0	
1. WET SCRUBBER AIR PRESSURE AT [POINT C]	FOUTLET	["H20"]	<u>.5</u>	<u> </u>	.5	
2. WET SCRUBBER DIFFERENTIAL PI [POINT B-C] Maintain between 1.0 and 4.5 inchi		["H2 0 "]	1.5	1.5	1.5	
1. FRESH WATER TO REACTOR		[gpm]	_X	_ <u>X</u>	_ <u>X</u>	
2. PETRO TO PRODUCT ON FILTER		[gpm]	3.5	3.5	3.5	
3. RINSE WATER TO PRODUCT ON FI	LTER	[gpm]	<u> 7.0 </u>	7.0	7.0	
RODUCT SCREEN ANALYSIS			SAMPLE	SAMPLE	SAMPLE	
+60			. 09	108	1 :1	
+100	•	less than 20]	8.5	11.2	12.1	
+200	•	less than 70]	48.2	59.	lele	
+325	-	less than 30]	22.8	18.3		
-325	l suonia pe	less than 10]	19.3	10.5	4.5	

REMARKS:

an an a'		C INDUSTRIES, LLA CONTROL AND PH		G	
DATE: <u>17/15/1</u> 1	LOT #: ///	-349	SFS OR P	FS PRODUCTIO	ON [circle one]
A OPERATOR:	HANCEY		SHIFT:	<u>Z</u>	
PRODUCT DRYING	START TIME: [* defined as the time	1515 e period that product p	asses through the d	STOP TIME: lrying column]	2110
	START TIME:	H GARGAR HELSEN AND MICHAELSE TO DUIT THE STORE		STOP TIME:	erinantianer achtiganer ann ann achtairte achainn an achtairte ann ann ann ann ann ann ann ann ann an
	START TIME:	10 10 11 11 11 11 11 11 11 11 11 11 11 1	ALEYETISLAMI, YALAYO TIYA	STOP TIME:	NTO GROWING LOW MADE OF THE REPORT OF THE WAY AND
		TIM	E 1	TIME 2	TIME 3
1. FLOWS ON TIME		144	17		
2. FILTER START TIME		151		PARTIE CONTRACTOR OF A STREET OF A STREET	r singeres the market for the second statement of the
3. FLOWS OFF TIME		200		Number of the state of the stat	Carbani (C. 1996), 1997, 1997, 1997, 1997, 1997, 1997, 1997, 1997, 1997, 1997, 1997, 1997, 1997, 1997, 1997, 19
4. SCREWS DOWN TIME		211	D		
5. TIME		16.	15	1815	۵٬۳۵۹ - ۲۰۰۵ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ ۱۹۰۳ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ - ۲۰۰۹ -
6. BURNER EXIT TEMP		M	4	NA	
7. DRYER EXIT TEMP		36	0	3.60	o (the state of the state of th
8. VENT FAN AMPS		_2		-25	
9. DRAFT FAN AMPS		7	Displace and displace structure	70	and the state of t
10. CHLORIDES		_/0.	0	9.5	
DOWN TIMES AND REASON	IS:				****
RAW MATERIALS USAGE	, FSA	na n		KCL	n n Bangaran na ang kang kang kang kang kang kang
TANK NUMBER:	4 FISH	oversame and the second second	N-201400euxy200400000000		
BEGIN OUTAGE:	.1º/2, "				an shara garan ya uga kufa sa na
END OUTAGE:	2'7"	<u>3" Pull</u> down REACTORS			~
USAGE:	18 1/2"	CTUTOCOLOGICAL CALCULAR CONTRACTOR	a second and find the second	1100000012 CTM	addrifted after press and the second
NUMBER OF LIQUID BRINE TR	RUCKS UNLOADED				
NUMBER OF SALT TRUCKS	UNLOADED:				
NUMBER OF ACID TRUCKS	UNLOADED:	2			

NUMBER OF KCL RAILCARS UNLOADED: TIME OF BATCHING PETRO

NUMBER OF ACID RAILCARS UNLOADED:

PETRO USED IN BATCHING

REMARKS: SHAKER SCREEN CONDITION AFTER LOADING TRAILER: PRODUCTION TRAILER INTERNAL CONDITION AFTER UNLOADING: 3-4 Jon's Stuck on stars.

DATE: 12-15-11 LOT #:	k11-349		PFS PRODUCTION	[circle one]
BOPERATOR: Sanders	,		FT: 204	
		SAMPLE	SAMPLE	SAMPLE
1. TIME		1615	1815	2015
2. PRODUCTION RATE Start plant at 105 tpd and go to 120- tpd once - 325 < 10%	[tpd]	100	100	A RECONTRACTOR OF A RECONSTRUCT OF A RECONST
3. ACID [FSA] FLOW	[gpm]	46	46	
4. ACID [FSA] SPECIFIC GRAVITY		1221	1221	
5. ACID [FSA] STRENGTH	%	24.75	2475	
6. KCL/SALT BRINE FLOW	[gpm]	46	46	Manufact with which we have a
7. KCL/SALT BRINE SPECIFIC GRAVITY		1199	1190	
8. COLOR OF BRINE		white	white	
[white, yellow, tan, brown] 9. COLOR OF ACID		yellow	Sollar	
[white, yellow, tan, brown]		<u> </u>	<u></u>	
10. REACTOR NO. 1 TEMP [PFS ONLY] Maintain between 110 and 140 degrees	[F]		2005	and the second
11. DRYER TEMPERATURE Maintain between 310 and 350 degrees	[F]	370	_ <u>580</u>	Wington gang and a subfict of the su
12. VACUUM READING	["Hg]		14	and the second
Maintain between 12 and 18 13. PRODUCT TEMPERATURE	[F]	283	291'	
14. VENTURI SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 50 AND 55 gpm	[gpm]	50	59	
15. VENTURI SCRUBBER AIR PRESSURE AT IN	VLET ["H20"]	_/		
[POINT A] 16. VENTURI SCRUBBER AIR PRESSURE AT O [POINT B]	UTLET ["H20"]	2	2	
17. VENTURI SCRUBBER DIFFERENTIAL PRES [POINT A-B] Maintain between 8 and 14 inches of water	SSURE ["H20"]	<u> </u>	4	Constant of the Constant of the American
18. WET SCRUBBER WATER FLOW RATE MAINTAIN BETWEEN 42 AND 47 gpm	[gpm]	42	42	The second s
19. WET SCRUBBER WATER PRESSURE MAINTAIN BETWEEN 20 AND 22 PSIG TO THE SPRAY NOZZLE	[psig]	21	21	
20. WET SCRUBBER AIR PRESSURE AT INLET [POINT B]	[′] ["H20"]	2	2	
21. WET SCRUBBER AIR PRESSURE AT OUTLI [POINT C]	ET ["H20"]			
22. WET SCRUBBER DIFFERENTIAL PRESSUR [POINT B-C] Maintain between 1.0 and 4.5 inches of water	~ -	1.5	1-5	An in the Physics of the physical states of the second states of the se
21. FRESH WATER TO REACTOR	[gpm]			
22. PETRO TO PRODUCT ON FILTER	[gpm]	3	3	anni a sha na sha na sha na sha na sha anna sha
23. RINSE WATER TO PRODUCT ON FILTER	[gpm]	6	10-	All Constant and C
PRODUCT SCREEN ANALYSIS		SAMPLE 17	15 SAMPLE 19	15 SAMPLE
+60		30 1	2 17 1	- •
	Should be less than 20]	11.8 11.	1 12.4 11	المسمانية ويسمين بالبرجيسة فيمانكا وماليك أشارك والمتحاط والبيا
-	Should be less than 70]	50.9 51	- And the second se	فيسجد بسما فمنفاط المستركات بطغان الشريقي فالمتحديثان كمجانبا فانجاز بالتكا
	Should be less than 30] Should be less than 10]	11 - 0	and the first of the second	2
** If you are not able to maintain the ab				diately
Condition of Y-Strainer?: ∂k		you have to Clean i		uidiciy.
REMARKS:		×		